4-95)	RM 3			LICENSEE EVENT DEDODT (LED)								ESTINA INFORM LEARN BACK ESTINA	AP-AOVED BY OMB NO. 3150-0104 EXPIRES 04/30/98 ESTEMATED BURDEN PER RESPONSE TO COMPLY WITH THIS MANDATORY INFORMATION COLLECTION REQUEST. 50.0 HRS. REPORTED LESSONS LEARRIED ARE INCORPORATED INTO THE LICENSING PROCESS AND FED BACK TO INDUSTRY. FORWARD COMMENTS REGARDING BURDEN ESTMATE TO THE INFORMATION AND RECORDS MANAGEMENT REACH IT. 5 F33). U.S. NUCLEAR REGULATORY COMMISSION, WASHINGTON, DC 20555-0001, AND TO THE PAPERWORK REDUCTION PROJECT (3150-0104), DFFICE OF MANAGEMENT ' 40 BUDGET, WASHINGTON, DC 20503.							
ACILITY	ACILITY NAME (1) Millstone Nuclear Power Station Unit 3													D	OCKET NUMB		PAGE (3)			
Millistone Nuclear Power Station Unit								int 3					05000423				1015			
TITLE (4)	Re	sidua	l Heat	Remo	val F	Pump	Sucti	ion Relief	Valve	Set	tpoint !	Not in	Acco	ord	ance Wit	h Technic	cal Sp	pecification	ns	
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On September 18, 1996 with the plant in Mode 5, during a review conducted by plant engineering personnel, it was determined that the actual setpoint for the Residual Heat Removal (RHR) pump suction relief valves was not in accordance with the requirements of Technical Specifications (TS). Contrary to the TS limit of 450 psig, the actual lift pressure for the RHR pump suction relief had been set at 440 psig. This condition was reported on October 18, 1996 pursuant to 10CFR50.73(a)(2)(i)(B) as an operation or condition prohibited by the plant's TS.

On August 29, 1997 with the plant in Mode 5, while performing a review of RHR suction relief valve surveillance test procedures, it was discovered that previous RHR relief valve calibrations were performed incorrectly resulting in the B train RHR relief valve setpoint being outside the tolerance allowed by the TS Limiting Condition for Operation. Consequently, this condition is being reported pursuant to 10CFR50.73(a)(2)(i)(B) as any operation or condition prohibited by the plant's TS.

The cause of the September 1996 event was attributed to insufficient configuration control within the design control program. The cause of the August 29, 1997, event was a deficiency in the relief valve setpoint testing program temperature correction data. As an immediate corrective action for the August 29, 1997 event, the B train RHR valve was declared inoperable, recalibrated to the correct setpoint and declared operable. The RHR setpoint calculation will be revised to properly incorporate the RHR pump suction relief valve temperature correction for the full temperature range. In addition, an evaluation of the RHR relief valve setpoint effect will be completed on the RHR pump discharge piping stress analyses.

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I. Description of Event

On September 18, 1996 with the unit in Mode 5, during a review conducted by plant engineering personnel, it was determined that the actual setpoint for the Residual Heat Removal (RHR) pump suction relief values was not in accordance with the requirements of Technical Specification Limiting Condition for Operation 3.4.9.3.a.2 and 3.4.9.3.a.3, "Reactor Coolant System - Overpressure Protection Systems." Technical Specifications (TS) require that the RHR pump suction relief be set at 450 pounds per square inch gauge (psig) in order to provide adequate over pressure protection when the temperature of any Reactor Coolant System (RCS) cold leg is less than 350 degrees Fahrenheit (°F). Contrary to this requirement the actual lift pressure for the RHR pump suction relief had been set at 440 psig. This condition was reported on October 18, 1996 pursuant to 10CFR50.73(a)(2)(i)(B) as an operation or condition prohibited by the plant's Technical Specifications.

On July 10, 1997, License Amendment 143 was incorporated resulting in an RHR relief valve setpoint of \ge 426.8 psig and \le 453.2 psig. On August 29, 1997, with the plant in Mode 5, while performing a review of RHR suction relief valve curveillance test procedures, it was discovered that previous RHR relief valve calibrations were performed incorrectly. The valve vendor requires a setpoint temperature correction factor of +3% when valves are used in 250°F or higher struce but are tested/set at ambient temperatures. This is to compensate for physical changes in the relief valve such spring loading, etc. The valves have always been tested and calibrated in this manner. At cold conditions (<250°F), the vendor's +3% temperature correction factor no longer applies. Since this relief valve must operate in both temperature ranges, this effectively narrows the setpoint acceptance tolerance to -0%, +3% or (440 to 453.2 psig) (See Figure 1).

A receive of the most recent RHR suction relief valve setpoint calibration records revealed that although the "A" relief valve had been calibrated to 453 psig (July 8, 1992), within the TS range, the E train RHR relief valve had been set to 455 psig (August 24, 1993), which was outside the TS setpoint tolerance range by 1.8 psig. Subsequently, between August 24, 1993 to the present, the Unit operated in a condition prohibited by the plant a Technical Specifications. This condition is therefore reportable pursuant to 10CFR50.73(a)(2)(i)(B).

II. Cause of Event

On March 26, 1985 during the construction of the unit, the Architect/Engineer (A/E) issued a design change, which lowered the setpoint for the RHR suction relief valve from 450 psig to 440 psig. This design change did not specify that a technical specification change was required. The design change was supported by the issuance of a setpoint calculation change on April 29, 1985. Subsequently, the plant Maintenance Department established the relief valve test program. In implementing the relief valve test program, insufficient information was extracted from design documents when establishing the appropriate temperature correction values for testing of valves contained within the program.

The cause of the August 29, 1997, event was a deficiency in the relief valve setpoint testing program. Inadequate management attention was applied to implementation of the relief valve test program during construction which led to an ineffective transfer of information between the engineering and maintenance departments. Engineering had included the KHR system maximum operating temperature, as opposed to the system operating temperature range, in various design documents. The Maintenance Department used this temperature information to determine the relief valve temperature correction factor not realizing that the valves are required to operate over temperature ranges rather than at a specific temperature. This led to the incorrect relief valve setpoint being implemented in the field.

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III. Analysis of Event

The unit has operated using the 440 psig setpoint as required by the original A/E design change and the associated setpoint calculation. The 440 psig setpoint is the technically correct setpoint for the RHR suction relief valves to ensure over pressure protection for the RHR piping in accordance with ASME requirements. Subsequent relief valve capacity calculations were based on the 440 psig setpoint. Over pressure protection of RHR piping and Low Temperature Over Pressure/Cold Over Pressure Protection System (LTOP/COPPS) requirements also have utilized the 440 psig setpoint for calculations performed following the initial design change.

For the August 1997 event regarding the 455 psig B RHR relief valve set pressure, the ability of the valve to function as a Cold Over Pressure Protection (COPPs) relief valve was demonstrated in an engineering calculation. A single RHR relief valve at a set pressure of 440 psig and 10% accumulation has sufficient capacity to limit reactor vessel pressure to 547 psig, which is below the 10CFR50 Appendix G "Fracture Toughness Requirements" overpressure limit of 558 psig. The TS setpoint range of 426.8 psig to 453.2 psig was selected based on a 440 psig setpoint and the ±3% opening pressure tolerance allowed by ASME III NC-7614.2(b), "Protection Against Overpressure - Popping Pressure Tolerance," for relief valve with set pressures > 70 psig. Therefore, an RHR relief valve which is set to the higher end of the TS range is considered to have a 440 psig setpoint and the 455 psig value is considered as only a 1.8 (455 minus 453.2) psig increase in this setpoint. Consequently, the maximum pressure limit of the reactor vessel was not challenged due to the 455 psig set pressure. As a result, the safety significance and consequences of an overpressure event occurring, while the B RHR valve was set outside the TS allowed range, were minimal.

The 455 psig B RHR relief valve set pressure also is expected to have a minimal effect on the RHR pump discharge piping stress analyses. The pump discharge design pressure of 600 psig is exceeded when the relief valve lifts. However, ASME III NC-3612.3 allows peak pressure during infrequent upset conditions to exceed design pressure if it can be shown that the peak pressure does not cause pipe wall stresses from exceeding allowable values. NU will confirm that peak pressure that would occur with the B RHR pump suction relief valve set at 455 psig would have no deleterious effect on the RHR pump discharge piping stress analysis.

IV. Corrective Action

As a result of the September 18, 1996 event, a Technical Specifications change was implemented on July 10, 1997 that revised the setpoint value identified in Technical Specifications 3.4.9.3.a.2 and 3.4.9.3.a.3 from 450 psig to \geq 426.8 psig and \leq 453.2 psig.

As an immediate corrective action for the August 29, 1997 event, the B train RHR was declared inoperable. After correcting the surveillance testing procedure to take into account the RHR relief valve's hot/cold settings and gauge accuracies the valve was calibrated to the correct setpoint.

Since plant construction, programmatic barriers have been implemented that provide assurance of adequate interdepartmental interface. For this instance, the specific issues that led to the inaccurate information being transmitted between departments and subsequently, being incorrectly implemented in the field are being addressed within the Millstone Corrective Action Program.

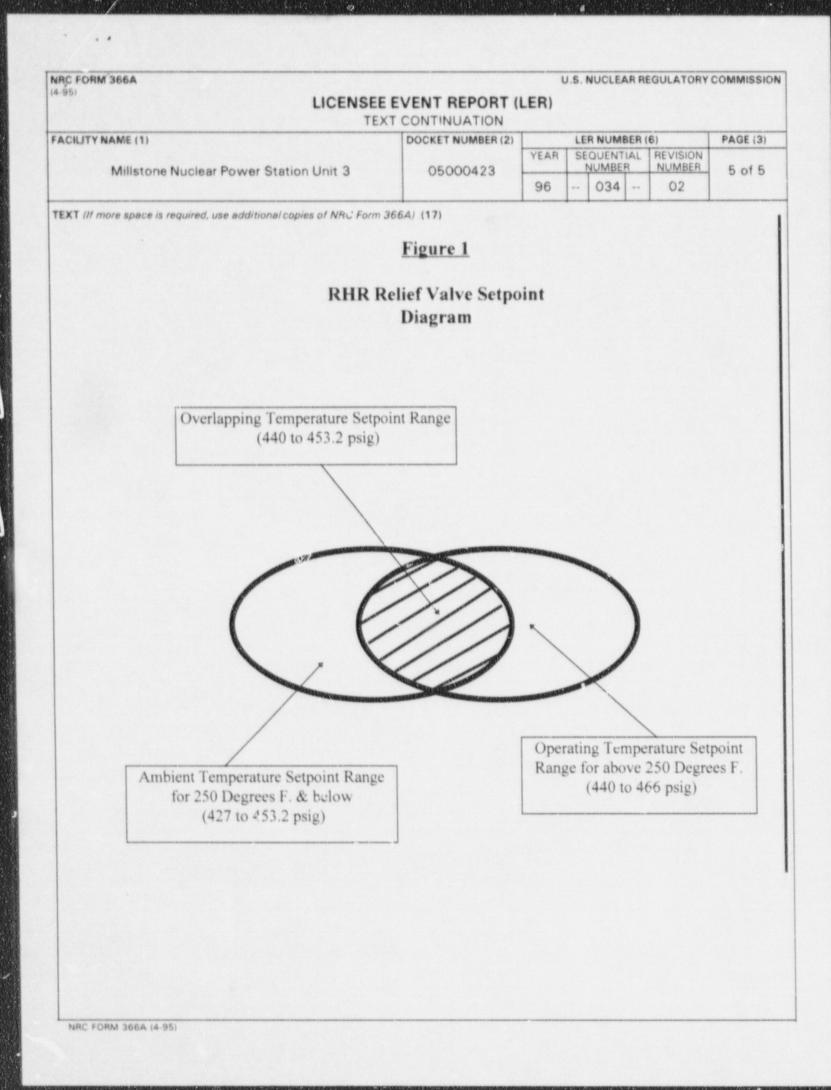
The following corrective actions will be performed:

 The setpoint calculation will be revised to properly incorporate the RHR pump suction relief valve temperature correction for the full temperature range prior to entry into Mode 4.

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4-95)	LICENSE	E EVENT REPORT (LER)								
		XT CONTINUATION									
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2. An evaluation entry into Mo	n of the RHR relief valve setpoint effe de 4.	ect on the RHR piping st	ress an	aly	ses will	be	completed	prior to			
V. Additional I	nformation										
None											
Similar Eve	nts										
Listed below are	historical LERs whose causes can b	e attributed to insufficier	at confi	aura	ation cr	ontro	within the	design			
	Many of these events were identifie			*							
LER 96-007-00	Containment Recirculation Spray, Quench Spray, and Safety Injection System Outside Design Basis Due to Design Errors										
LER 96-009-02	Inoperable Shutdown Margin Monito	ore from Low Count Rate	Duet		adequa	te D	esian Cont	m			
LER 96-013-00	Residual Heat Removal System De										
LER 96-026-02	Non-Conservative Primary Grade										
LER 97-003-00	Potential For Recirculation Spray S										
LER 87-003-00	Restarting During Accident Condition		ne Due	10	NOO F	cum	stopping				
LER 97-015-00	Potential Vortexing of Recirculation										
LER 97-021-00	Defective Design of RSS Expansio		,								
LER 97-028-00	Potential Loss of Net Positive Sucti			Su	tom D	imo	e				
LER 97-028-00	Design Basis Concern on EGTR Ar		Toplay	Sy:	stempt	ump	5				
LER 97-029-00			Cathle				alu				
	RHR Valve Low Pressure Open Pe							AAA Torm			
LER 97-035-00	Potential Nonconservatism for Stea	am Generator water Leve	DI LOW-I	LOW	Trip Se	etpo	int Due to P	'MA Term			
LER 97-046-00	Uncertainties Containment Recirculation Spray S	ystem Cubicle Flood Pot	ential								
Manufactu	rer Data										
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Valve, Relief		RV									
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