N-4080-027 Suppl A&B Rev O: MSLB Containment P/T

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Calculation No. N-4080-027 - SUPPLEMENT B

Sheet No. B-2

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1.0 PURPOSE

1.1 TASK DESCRIPTION

The purpose of this Supplement B is to provide a new calculation of the Containment P/T response to the design basis Main Steam Line Break (DB MSLB) event consistent with the Licensing Basis of SONGS Units 2 and 3 (reference 6.2), where the pre-MSLB initial containment pressure is the nominal atmospheric value (14.7 psia) used in prior UFSAR containment functional design. The results of this Supplement B will become the Analysis of Record (AOR) for the design basis MSLB as it applies to containment functional design. Supplement B will also serve as the AOR for calculation of peak post-MSLB containment pressure with the initial containment pressure at 1.5 psig, documenting the existence of peak pressure margin under maximum containment initial pressure conditions [Technical Specification maximum value of 16.2 psia (1.5 psig) per LCO 3.6.1.4].

The prior analysis of reference 6.1 will remain valid for the purposes of defining the input modelling for the design basis MSLB containment P/T analysis for all parameters except those minor changes identified below.

Supplement B incorporates the following changes in the containment heat removal spray system performance parameters:

- 1.1.1 The containment injection mode spray flow rate is reduced to 1600 gpm, bounding the lowest calculated minimum injection spray flow with 7.5% degraded containment spray pumps (reference 6.3).
- 1.1.2 The emergency air cooling unit (ECU) start time is delayed to coincide with the start time of full containment spy flow at 50 seconds. This change will add 35 seconds to the currently calculated post-MSLB start start time for the ECUs without loss of power (reference 6.14) with negligible penalty in containment P/T response and provide margin for the future changes in ECU start time.

The MSLB evaluated in this calculation continues to be the design basis 7.48 ft² steam line break accident at 102% power with off-site power available and with a loss of one train each of containment emergency air coolers and containment sprays.

Bechtel Standard Computer Code NE100, Release G1-15 (COPATTA) (reference 6.5), on the Nuclear Fuels Engineering IBM-RISC workstation system will be used in this calculation to evaluate the containment pressure and temperature transients for the DB MSLB.

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Subject CONTAINMENT P/T DESIGN BASIS MSLB Sheet No. B-5

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1.2 CRITERIA, CODES and STANDARDS

The criteria, codes and standards applicable to the Containment P/T Analysis for Design Basis MSLB (reference 6.1), are also generally applicable in this analysis. The applicable regulatory design criteria include:

- General Design Criterion (GDC) 16, "Containment Design"
- General Design Criterion (GDC) 38, "Containment Heat Removal"
- General Design Criterion (GDC) 50, "Containment Design Basis".

The applicability of these criteria to peak containment pressure and temperature are described in detail in Reference 6.1.

The containment design pressure and temperature are 60 psig and 300 °F per the Technical Specifications (references 6.5, 6.6, 6.7 Section 5.2.2) respectively.

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Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B

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2.0 RESULTS/CONCLUSIONS AND RECOMMENDATIONS

2.1 RESULTS/CONCLUSIONS

2.1.1 Initial Containment Pressure @ 0 PSIG

Figures 2-1 through 2-7 show the analysis results out to 10,000 seconds, which is well beyond the time of the affected steam generator dry-out and termination of significant mass and energy release into the containment (71.08 seconds). At 10,000 seconds, the containment temperature and pressure are well below the peak values and decreasing. Section 10 contains tabulated conditions to the end of the transient calculation at 1E+4 seconds, at which time the refueling water storage tank would have been depleted and operator action to place RCS on shutdown cooling for decay heat removal would have been underway.

Figure 2-1 presents the containment gauge pressure versus time for the CONTAINMENT P/T DESIGN BASIS MSLB. The plot in Figure 2.1 is generated using the data presented in Section 10.1.

Figure 2-2 presents the sump and vapor temperatures versus time for the CONTAINMENT P/T DESIGN BASIS MSLB. The plots in Figure 2.2 are generated using the data presented in Section 10.1.

Figure 2-3 presents the condensing heat transfer coefficient v.s. time used by the COPATTA Code during the DBMSLB. The plot in Figure 2.3 is generated using the data presented in Section 10.1.

Figure 2-4 presents the inside surface temperature of heat sink 1 (reactor building dome, painted steel liner plate) to represent the maximum post-MSLB temperature of the containment structure. The plot in Figure 2.4 is generated using the data presented in Section 10.1.

Figure 2-5 presents the integrated energy transferred from the containment vapor region by one train of air coolers, two Emergency Cooling Units (2ECUs) and one train of containment spray as a function of time. The plots in Figure 2.4 are generated using the data presented in Section 10.2. The ECUs transfer vapor energy to the component cooling water system (CCWS) which transports the energy outside the containment. The containment sprays are operating in the injection mode and transfer vapor energy to the containment sump region as hot water.

Figure 2-6 presents the integrated heat transfer of the air coolers and containment sprays. The plots prsented in Figure 2.6 are generated using the data tabulated in Section 10.2

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Figure 2-7 presents the rate of energy transfer from the vapor region by a single train of emergency cooling units (2ECUs) and by a single train of containment sprays as a function of time. The plots in Figure 2.5 are generated using the data presented in Section 10.2.

Table 2-1 presents the containment P/T Design Basis MSLB accident chronology with Initial Containment Pressure CPi = 14.7 psia (0 psig).

The calculated peak pressure of 56.6 psig is less than the 60 psig design pressure and also less than the previously identified peak pressure (58.5 psig) in the prior AOR (N-4080-027, reference 6.1). The decrease in the peak pressure is attributed to the change in the initial containment pressure from 1.5 psig to 0 psig.

The calculated peak vapor temperature of 427.7°F is greater than the 300°F design temperature, however the duration of the event is sufficiently brief to prevent heating of the containment structural materials beyond the design limits. The thermal response of the 0.25" thick containment steel liner plate to the MSLB environment shown in figure 2-4 presents a conservative example of the transient heating of the containment structure during the accident. As shown in the figure, the liner plate remains below 250 °F during the MSLB event.

The peak vapor temperature is about 7°F greater than the previously identified peak temperature in the prior AOR (N-4080-027, reference 6.1). The increase in the peak temperature is primarily attributed to the lower containment initial pressure (O psig) compared to that in the prior analysis at 1.5 psig. The lower air inventory reduces the total containment heat capacity resulting in a small increase in short-term peak vapor temperature [see BN-TOP-3, Revision 4, Section 4.1.2 and Table 15 (reference 6.8)]. The delay in ECU start time from 15 to 50 seconds also adds slightly to the increase in peak vapor temperature as compared to the prior analysis.

Subject CONTAINMENT P/T DESIGN BASIS MSLB

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2.1.2 Initial Containment Pressure @ 1.5 PSIG

Table 2-2 presents the CONTAINMENT P/T DESIGN BASIS MSLB accident chronology with Initial Containment Pressure CPi = 16.2 psia.

The calculated peak pressure of 58.7 psig is less than the 60 psig design pressure but slightly greater than the previously identified peak pressure (58.5 psig) in the prior AOR (N-4080-027, reference 6.1). The increase in the peak pressure is attributed to the changes in the CSS flow rate and ECU start delay time.

The calculated peak vapor temperature of 421.6°F is greater than the 300°F design temperature, however the duration of the event is sufficiently short enough to prevent heating of the containment structural materials beyond the design limits. The peak vapor temperature with the initial containment pressure at 1.5 psig is about 6.1°F lower than for the case with the initial pressure at 0 psig due to the greater containment heat capacity which exists at the higher initial containment pressure.

The peak vapor temperature is about $0.6^{\circ}F$ greater than the previously identified peak temperature in the prior AOR (N-4080-027, reference 5.1). The slight increase in peak temperature is attributed to the delay in ECU start time from 15 to 50 seconds.

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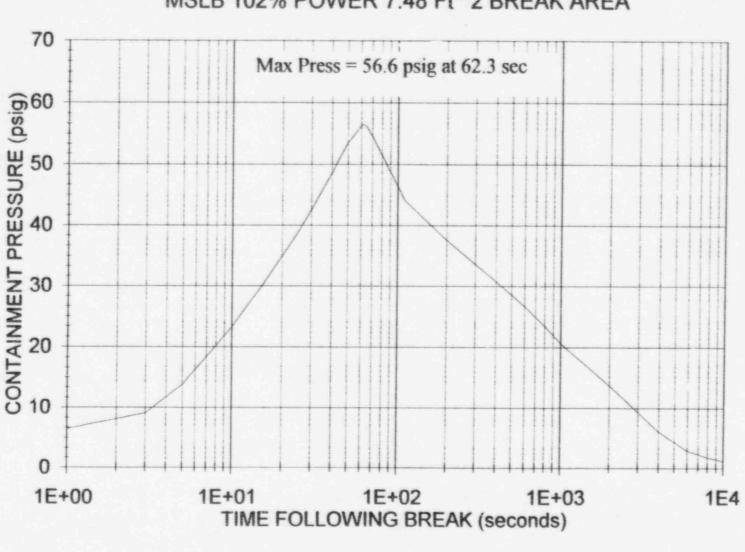
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FIGURE 2-1: PRESSURE MSLB 102% POWER 7.48 Ft**2 BREAK AREA



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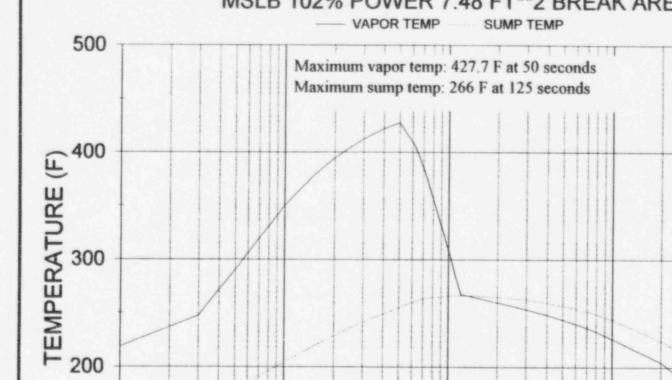
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FIGURE 2-2: TEMPERATURE MSLB 102% POWER 7.48 FT**2 BREAK AREA

1E+02

TIME FOLLOWING BREAK (seconds)

1E+03



1E+01

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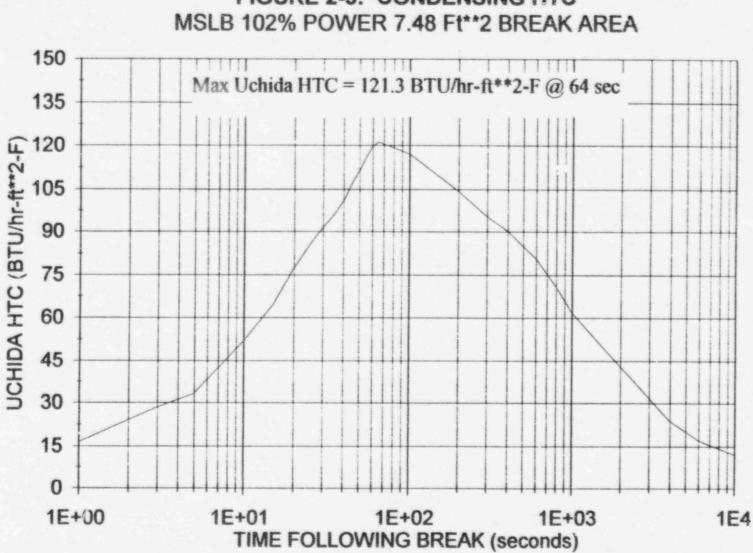
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FIGURE 2-3: CONDENSING HTC



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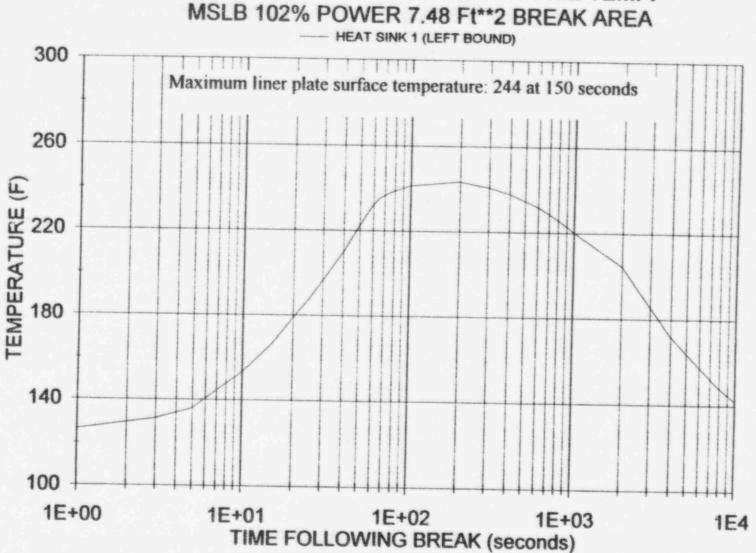


FIGURE 2-4: LINER PLATE SURFACE TEMP.

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FIGURE 2-5: ENERGY

MSLB 102% POWER, 7.48 FT**2 BREAK AREA

TOTAL

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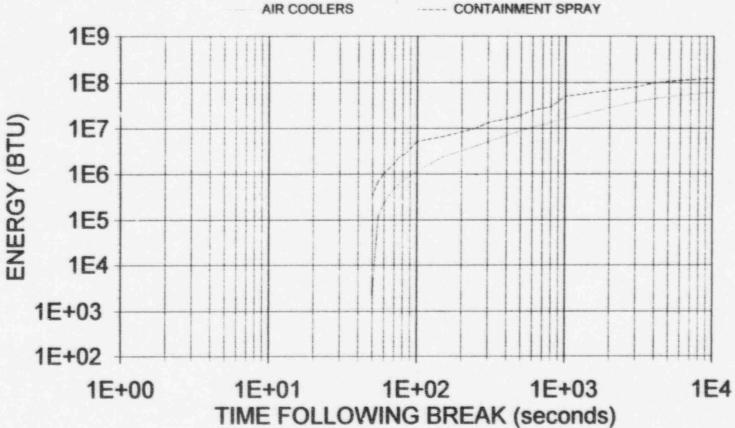
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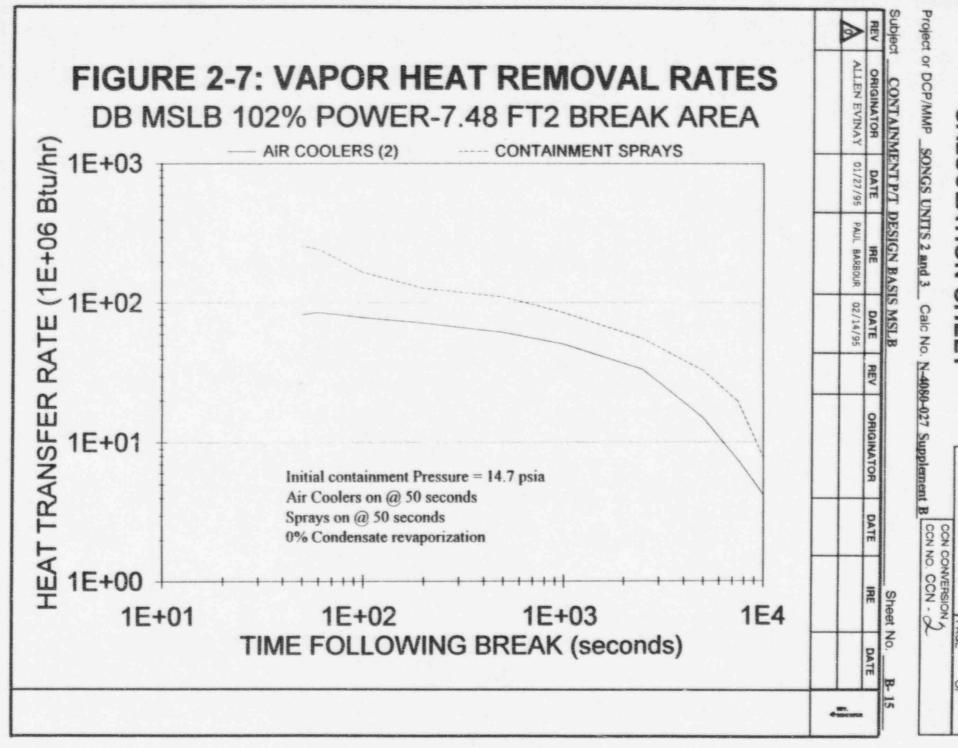
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FIGURE 2-6 ENERGY MSLB 102% POWER, 7.48 FT**2 BREAK AREA AIR COOLERS CONTAINMENT SPRAY





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Table 2-1

CONTAINMENT P/T DESIGN BASIS MSLB EVENT CHRONOLOGY

Initial Containment Pressure CPi = 14.7 psia

TIME (seconds)	EVENT
0.0	MSLB Occurs
50	Containment Sprays Start (Nozzles at Full Discharge Flow) AND Emergency Fan Coolers Start (Full capacity)
50	Peak Containment Temperature of 427.7 °F reached
62.2	Peak Containment Pressure of 56.6 psig reached
71.08	End of Blowdown (Affected Steam Generator)
175.0	Containment Liner Plate Maximum Temperature of 243.8 °F reached
9000.0	Maximum Tech. Spec. Containment Pressure of 1.499 psig ≤ 1.5 psig reached
10,000.0	End of Analysis

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Table 2-2

CONTAINMENT P/T DESIGN BASIS MSLB EVENT CHRONOLOGY

Initial Containment Pressure CPi = 16.2 psia

TIME (seconds)	EVENT
0.0	MSLB Occurs
50.0	Containment Sprays Start (Nozzles at Full Discharge Flow) AND Emergency Fan Coolers Start (Full capacity)
50.0	Peak Containment Temperature of 421.6 °F reached
62.3	Peak Containment Pressure of 58.7 psig reached
71.08	End of Blowdown (Affected Steam Generator)
200.0	Containment Liner Plate Maximum Temperature of 242.8 °F reached
10,000.0	End of Analysis

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2.2 RECOMMENDATIONS

This Supplement B provides a new analysis of record for the containment pressure and temperature response to the Design Basis MSLB event for containment functional design as reported in Section 6.2 of the UFSAR. The new analysis does not apply to in-containment equipment qualification which is separately addressed by Supplement A of the base calculation. Supplement B also provides analysis for the determination of peak post-MSLB pressure margin starting with the maximum initial containment pressure conditions (Technical Specification maximum value of 16.2 psia (1.5 psig per LCO 3.6.1.4)).

Section 6.2 of the UFSAR will be revised to replace the detailed results of the old AOR (initial containment pressure at zero psig) with the results of the new AOR for the same initial containment pressure of zero psig. Text will be added to clarify that analyses were also done with the initial containment pressure at 1.5 psig to confirm that the peak post-MSLB pressure remains below the containment design value of 60 psig when the initial pressure is at the Technical Specification maximum LCO value of 1.5 psig.

Technical Specification LCO/SRs 3/4.6.1.1, 3/4.6.1.2, and 3/4.6.1.3 will be revised to incorporate the P_a of 56.6 psig from the new AOR; the value of P_t (one-half P_a) will be revised to 28.3 psig. Technical Specification Basis 3/4.6.1.4 will be revised to identify the peak pressure of 58.7 psig calculated with the initial containment pressure at 1.5 psig, demonstrating compliance with the containment design value of 60 psig. Technical Specification Basis 3/4.6.1.6 will be revised to identify the maximum steam line break containment pressure of 56.6 psig as calculated by the current AOR.

The prior containment P/T response analysis contained in N-4080-027 Revision 0, remains applicable only for the purposes of defining the input modelling for the DB MSLB containment P/T analysis for all parameters except those changes identified in this Supplement B to the calculation.

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3.0 ASSUMPTIONS

The assumptions used in this calculation are identical to those used in the prior Containment P/T Analysis for Design Basis MSLB (reference 6.1), except where noted. Reference 6.1 remains valid for the purposes of defining the input modelling for the DB MSLB containment P/T analysis for all parameters except those changes identified in this Supplement B to the calculation. The assumptions in reference 6.1 are arranged in groups which parallel the COPATTA Code card series data input. The modifications to reference 6.1 assumptions are listed below.

3.1 CARD SERIES 1

3.1.a ITEM 5: CONTAINMENT INITIAL TEMPERATURE

In both the AOR (reference 6.1) and this analysis, the containment initial temperature was assumed to be $120^{\circ}F$. This is the maximum average containment temperature per SONGS Units 2 and 3 Technical Specification LCO 3.6.1.5 (references 6.6 and 6.7).

3.1.b ITEM 11: CONTAINMENT HEAT SINK REVAPORIZATION FRACTION

This analysis is performed for Containment P/T Design Basis MSLB Temperature and Pressure profile generation and supports containment functional design and not in-containment equipment qualification. Therefore credit for revaporization of heat sink condensate will not be taken. Supplement Aa to the base calculation contains the MSLB analysis supporting equipment qualification.

3.2 CARD SERIES 5

3.2.a ITEM 3: CONTAINMENT EMERGENCY AIR COOLER START TIME

In the AOR (reference 6.1), the containment air cooler start delay time was identified as 15 seconds in the Design Input 4.3.a. In the present analysis the air cooler start time has been increased to 50 seconds to coincide with the containment spray actuation time. The emergency air cooling units have relatively little impact on short-term containment pressure and temperature, and by adding 35 seconds delay to ECU initiation, margin is added to accommodate potential changes in the timing of ECU startup. For example, based on the methodology contained in calculation N-4080-003 (reference 6.15), the 50 second start time for the ECUs is equivalent to assuming a 47-second stroke time for the CCW block valves that supply cooling water to the air coolers, if all other parameters affecting ECU start time were to remain unchanged.

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Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B

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4.0 DESIGN INPUT

The design inputs used in this calculation are identical to those used in the prior Containment P/T Analysis for Design Basis MSLB (reference 6.1), except where noted. Reference 6.1 remains valid for the purposes of defining the input modelling for the DB-MSLB containment P/T analysis for all parameters except those changes identified in this Supplement B to the calculation. The assumptions in reference 6.1 are arranged in groups which parallel the COPATTA Code card series data input. The modifications to reference 6.1 assumptions are listed below.

4.1 CARD SERIES O

The last four zero entries on this card are deleted. The G1-15 (RISC) version of COPATTA does not utilize these data entry locations.

4.2 CARD SERIES 1

a. ITEM 2: PROBLEM RUN TIME

The appropriate problem run time is 10,000 seconds (~2.8 hours). The pipe break mass and energy release into the containment provided by the Combustion Engineering (ABB-CE) included on CARD SERIES 301 terminate at 71.08 seconds, when dryout of the affected steam generator is calculated to occur for this Design Basis MSLB event. This run time of 10,000 seconds is well past the end of significant mass and energy release into the containment. Generally a run time of 1000 seconds is adequate to show that the containment pressure and temperature are decreasing rapidly and well below the peak values calculated prior to steam generator dryout. For this calculation, however, the run time has been extended to 10,000 seconds to be consistent with the prior AOR. The 10,000 second run time also roughly coincides with the time at which the refueling water storage tank would become depleted by the operation of a single spray train. Containment spray would be discontinued when the RWST is empty, since the shutdown heat exchanger, normally used for cooling recirculated spray water from the sump, would be required for shutdown cooling of the RCS.

b. ITEM 3: INITIAL CONTAINMENT PRESSURE

Consistent with the original design basis containment P/T response analysis for MSLB reported in the UFSAR supporting containment functional design (UFSAR Section 6.2), and SONGS Units 2 and 3 licensing basis (reference 6.2), the initial containment pressure will be set to 14.7 psia (0 psig). Sensitivity studies in Bechtel Topical report BN-TOP-3 (reference 6.8) show that the short-term peak vapor temperature increases with decreasing initial containment pressure because lower initial pressure corresponds to a smaller initial air mass in containment and a corresponding smaller containment total heat capacity.

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Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B CCN CONVERSION 2

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The Supplement B also provides an analysis for the detrmination of peak post-MSLB containment pressure where the initial containment pressure is set at the Technical Specification maximum value of 16.2 psia (1.5 psig per LCO 3.6.1.4).

4.3 CARD SERIES 5

The last two entries on this card (0 and 105) are deleted. The G1-15 (RISC) version of COPATTA does not utilize these entry locations

4.3.a ITEM 3: CONTAINMENT EMERGENCY AIR COOLER START TIME

In the present analysis, the air cooler start delay time has been increased from 15 seconds to 50 seconds to coincide with the containment spray actuation time. The increase in air cooler start delay time will provide margin to accommodate potential changes in the timing of ECU startup such as an increase in the stroke time of the CCW block valves that isolate the cooling water from the air coolers.

CARD SERIES 301 4.4

No changes are made to card series 301 input which provides the mass flow rate and fluid enthalpy entering the containment from the main steam line break. The data is for the Design basis MSLB at 102% power with a break area of 7.48 ft2.

As documented by CCN 1 to N-4080-004 (reference 6.3) and CCN 1 to N-4080-007 (reference 6.13), single failure of one of the isolation valves (HV8200 and/or HV8201) on the steam line feeding the auxiliary feed water pump turbine could allow cross-flow of steam from the intact steam generator into the containment through the affected steam generator. This cross-flow would come from the 1" diameter bypass lines installed around steam line check valves 1301MU003 and 1301MU005 by MMP 2 & 3 6869.00SM. This potential additional mass and energy input is not included in this new AOR. The referenced CCNs demonstrate that the effect of the cross-flow on short-term peak containment conditions is not significant. The increase in peak pressure and peak temperature due to this potential cross-flow are less than 0.1 psi and 0.3°F, respectively.

Similarly, a single failure of the containment isolation valve on instrument air or high/low nitrogen supply lines to close, coupled with a MSLB-induced failure of one of the supply or distribution lines inside the containment would also lead to additional mass and energy release beyond what is provided by ABB-CE. CCN 2 to N-4080-007 (reference 6.13) evaluated this single failure and concluded that there would be no significant impact to the short-term peak containment pressure or temperature. Therefore, the mass and energy releases from a failed air or nitrogen line is not included in this Design Basis MSLB AOR.

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CCN CONVERSION

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B CON NO. CCN - 2

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4.5 CARD SERIES 801

No changes are made to card series 801 input except:

a.2(a) Containment Spray Injection Mode Spray Flow Rate

The minimum Containment Pump Spray Flow Rate has been changed to 1606 gpm (reference 6.3). In this Supplement B the value has been rounded down to 1600 gpm providing a small margin over the minimum predicted spray flow. Using the same criteria as in the AOR, this value translates to a flow rate of 7.956E+5 lb/hr for 100°F water coming from the RWST.

The containment spray flow would be discontinued at about 1E4 seconds, consistent with a calculated time to deplete the refueling water storage tank inventory, using a single spray train, of about 1.1E4 seconds (reference 6.1, section 4.5.b.1). Following spray termination, containment heat removal is provided by the continued operation of the single train emergency air cooler units (2ECUs). Long-term RCS decay heat removal for the DB MSLB would be provided by placing the RCS on shutdown cooling.

4.6 CARD SERIES 1101

The G1-15 (RISC) version of COPATTA does not have the option of multiple tables of ECU performance versus containment temperature for various values of cooling water supply temperature. Therefore, following the card series identifier (\$LIST POOL=1101), the input consists data pairs of containment saturation temperature and ECU heat removal rate.

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CCN CONVERSION

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B CCN NO. CCN -

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5.0 METHODOLOGY

The MSLB for Equipment Qualification evaluated in this calculation is the design basis $7.48~{\rm ft}^2$ steam line break accident at 102% power with off-site power available and with a loss of one train each of containment emergency air coolers and containment sprays.

The evaluation used the Bechtel COPATTA computer code (reference 6.5) to simulate the containment response to the MSLB.

The methodology employed in this calculation is identical to the present AOR (reference 6.1) for the Containment P/T Design Basis MSLB, with the exception that two different pre-MSLB containment pressure conditions are analyzed:

- Initial Containment Pressure of 14.7 psia (reference 6.2) for containment P/T functional design.
- 2) Initial Containment Pressure of 16.2 psia, maximum Technical Specification value, for peak post-MSLB containment pressure margin determination.

Small reductions in containment spray flow have been made to provide some margin with respect to currently calculated minimum values. In addition, the start time of the emergency air cooling units (ECUs) has been arbitrarily delayed to coincide with the start of containment spray to provide future margin on the timing of ECU startup.

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CON CONVERSION

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B CCN NO. CCN - X

Subject CONTAINMENT P/T DESIGN BASIS MSLB Sheet No. B-24 REV ORIGINATOR DATE IRE DATE REV ORIGINATOR DATE IRE DATE ALLEN EVINAY 01/27/95 PAUL BARBOUR 02/14/95

6.0 REFERENCES

- 6.1 SONGS Units 2&3 Calculation N-4080-027, Revision 0, "Containment P/T Analysis for Design Basis MSLB", January 13, 1994.
- 6.2 Memo from J.L. Rainsberry to A.J. Brough, "Peak Containment Pressure Calculations, San Onofre Nuclear Generating Station, Units 2 and 3", May 12, 1994.
- 6.3 SONGS Units 2&3 Calculation M-0014-009, Revision 0, Supplement A, "Containment Spray (CSS) In Service Minimum Requirements, July 28, 1994.
- 6.5 Bechtel Standard Computer Program, NE100, COPATTA, Version G1-15, "Containment Temperature and Pressure Transient Analysis", User and Theory Manuals.
- 6.6 SONGS Unit 2 Operating License and Technical specifications, up to and including Amendment 114.
- 6.7 SONGS Unit 3 Operating License and Technical specifications, up to and including Amendment 103.
- 6.8 Bechtel Topical report BN-TOP-3, Revision 4, "Performance and Sizing of Dry; Pressure Containments", March 1983.
- 6.12 SONGS Units 2 and 3 Calculation M-0072-036, Revision 0, "Containment Emergency Cooler Performance Verification", December 9, 1993.
- 6.13 SONGS Units 2 and 3 Calculation N-4080-007, Revision 2, "Containment Pressure and Temperature from MSLB at various Power Levels", April 21, 1983 (includes CCNs 1 and 2).
- 6.14 SONGS Units 2&3 Calculation N-4080-027, Revision 0, Supplement A "Containment P/T Design Basis MSLB For Equipment Qualification", November 4, 1994.
- 6.15 SONGS Units 2 and 3 Calculation N-4080-003, Revision 5, "Containment Spray (CSS) and Emergency Cooling Unit (ECU) Actuation Times", December 23, 1993

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7.0 NOMENCLATURE

Abbreviations are defined when first used within the body of the text.

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CCN CONVERSION

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B CCN NO. CCN - 2

Subject CONTAINMENT P/T DESIGN BASIS MSLB

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8.0 CALCULATIONS

8.1 COPATTA CODE INPUT DATA - Initial Containment Pressure CPi = 14.7 psia

COPATTA input data for the Containment P/T Design Basis MSLB Analysis for uses the current AOR (reference 6.1) input data with modifications to reflect changes in containment spray flow rate (reference 6.3), initial containment pressure and Air Cooler start time to generate containment temperature and pressure profiles for the containment P/T design basis MSLB. Only the changes to the reference 6.1 input data will be presented in the following subsections.

8.1.1 TITLE CARD

*DBMSLB 102%P, Pi=14.7, EV=0%, CT=1, TC=50, LOP=0, CS=1600, N-4080-027-SUP-B

8.1.2 CARD SERIES O

No changes made to Card Series O of reference 6.1 other than the deletion of the last four zero entries on the Bechtel input file as non-applicable to COPATTA version G1-15.

8.1.3 CARD SERIES 1: General Problem Information

&LIST POOL=1,1E5,14.7,2.305E6,120,0.6,20,582.945,1,1,0.00,14.7,0,0.50 \$END

ITEM 2:

TNFL = 2E4 seconds (per 4.2.a)

ITEM 3:

PAIR = 14.7 psia

The initial containment pressure before the MSLB mass and energy release is set to 14.7 psia for DB-MSLB for containment P/T finctional design (UFSAR Section 6.2), as discussed in the Design Input Item 4.2.b.

Card Series input ITEMS 4 through 10 remain unchanged from that of reference 6.1.

ITEM 11: EVAP = 0.0

The fraction of heat sink condensate which will be allowed to revaporize is set to 0.0. NO credit for revaporization will be taken for the purposes of DB MSLB analysis per assumption 3.1.a.

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CCN CONVERSION A

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B CCN NO. CCN - C

Subject CONTAINMENT P/T DESIGN BASIS MSLB

Sheet No. B- 27

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8.1.4 CARD SERIES 5: Air Cooler Information

\$LIST POOL=5,2,50,1E7,0,0 \$END

ITEM 3:

This item reflect the change of Containment Air Cooler start time from 15 seconds to 50 seconds as discussed in Design Input Item 4.3.a. No other changes have been made to this card data.

8.1.5 CARD SERIES 801: (Table 9)

This Card Series reflect the change of Containment Spray System (CSS) Flow Rate from 1612 gpm to 1600 gpm and the termination of containment spray flow at 10,000 seconds.

\$LIST POOL=801,

0, 0, 0, 0, 100. 100. 50, 0, 0, 0, 100. 100. 0, 0, 50, 7.956E5, 100. 100. 0, 0, 1E4, 7.956E5, 100, 100. 0, 1E4, 0.0, 0, 100, 100, 0, 0. 100 \$END 2E7, 0.0, 100.

8.1.6 CARD SERIES 1101

Items 2,3 and 4 of reference 6.1 input are deleted as not applicable to the G1-15 (RISC) version of COPATTA.

All other input used in this calculation remain unchanged from that of Reference 6.1, as described in Sections 8.1.1 through 8.1.33, except as changed in the preceding paragraphs.

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CCN CONVERSION

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B CCN NO. CCN - &

Subject CONTAINMENT P/T DESIGN BASIS MSLB Sheet No. B-28 REV ORIGINATOR DATE IRE DATE REV ORIGINATOR DATE IRE DATE ALLEN EVINAY 01/27/95 PAUL BARBOUR 02/14/95

8.2 COPATTA CODE INPUT DATA - Initial Containment Pressure CPi = 16.2 psia

Supplement B also provides additional analysis to determine the margin for peak post-MSLB containment pressure under maximum containment initial pressure conditions [Technical Specification maximum value of 16.2 psia (1.5 psig) per LCO 3.6.1.4]. COPATTA input data for the this case is presented as changes made to the COPATTA input for Containment P/T Design Basis MSLB Analysis and Equipment Qualification, presented in Section 8.1 of this document.

8.2.1 TITLE CARD

*TSMSLB 102%P, Pi=16.2, EV=0%, CT=1, TC=50, LOP=0, CS=1600, N-4080-027-SUP-B

8.2.2 CARD SERIES 0

No changes made to Card Series 0 of reference 6.1 other than the deletion of the last four zero entries on the Bechtel input file as non-applicable to COPATTA version G1-15.

8.2.3 CARD SERIES 1: General Problem Information

&LIST POOL=1,1E5,16.2,2.305E6,120,0.6,20,582.945,1,1,0.00,14.7,0,0.50 \$END

ITEM 3: PAIR = 16.2 psia

The initial containment pressure before the MSLB mass and energy release is set to 16.2 psia for the peak post-MSLB containment pressure analysis, as discussed in the Design Input Item 4.2.b.

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CCN CONVERSION CCN NO. CCN - 2

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B

Subject CONTAINMENT P/T DESIGN BASIS MSLB Sheet No. B-29 REV ORIGINATOR DATE IRE DATE REV ORIGINATOR DATE IRE DATE ALLEN EVINAY 01/27/95 PAUL BARBOUR 02/14/95 i g 9.0 COPATTA INPUT FILES 9.1 DBMSLB CPi = 14.7 psia *DBMSLB 102%P, Pi=14.7, EV=0%, CT=1, TC=50, LOP=0, CS=1600, N-4080-027-SUP-B \$LIST POOL=0,0,1,0,1 \$END \$LIST POOL=1,1E5,14.7,2.305E6,120,0.6,20,582.945,1,1,0.00,14.7,0.5 \$END LIST POOL=2,0,0,0,0,0,120,2E7 \$END \$LIST POOL=3,0,0,0,0,0,2E7,0,0,0,0 \$END \$LIST POOL=4,0,0,0,0,0,0,0,0,0,0,0,0 \$END \$LIST POOL=5,2,50,1E7,0,0 \$END \$LIST POOL=6,0,0,0 \$END \$LEAK NOPEN=0 \$END \$LIST POOL=101, 0, 0, 2E7, 0 SEND \$LIST POOL=201, 0, 0, 2E7, O SEND \$LIST POOL=301. 0. 5.145520E7, 1.195589E3, 0.22, 4.869032E7, 1.197482E3. 0.42. 4.622234E7, 1.198466E3. 0.62. 4.405936E7. 1.199410E3. 1.08, 4.003276E7. 1.201595E3. 1.58. 3.688855E7. 1.201757E3, 2.08. 3.445970E7. 1.202018E3, 2.58, 3.326288E7. 1.200986E3. 3.58. 3.152606E7, 1.201058E3, 4.58. 3.028468E7, 1.201655E3, 5.58. 2.940080E7. 1.201123E3. 6.58. 2.874870E7. 1.201126E3. 7.58. 2.706574E7. 1.204404E3. 8.58. 2.468326E7. 1.204367E3. 9.58, 2.294968E7, 1.204238E3. 10.58. 2.160122E7. 1.203908E3. 12.58, 1.943143E7. 1.203195E3. 1.765940E7, 14.58. 1.202277E3, 16.58, 1.637240E7. 1.201556E3. 18.58. 1.544720E7. 1.200963E3, 20.58. 1.473293E7, 1.200422E3. 25.58. 1.327525E7, 1.198820E3. 30.58, 1.221858E7, 1.197825E3. 35.58. 1.146406E7. 1.196753E3. 1.059131E7, 40.58. 1.195307E3. 45.58. 9.801216E6. 1.194165E3.

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CCN CONVERSION

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CCN CONVERSION CCN NO. CCN -

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B

Subject CONTAINMENT P/T DESIGN BASIS MSLB Sheet No. B- 32 REV ORIGINATOR DATE IRE DATE REV ORIGINATOR DATE IRE DATE ALLEN EVINAY 01/27/95 PAUL BARBOUR 02/14/95 6 1 20, 0.23028, 37, 1.00110. 21, 4.06363 \$END \$LIST POOL=101201, 4, 1, 5, 2, 2, 2, 2 \$END \$LIST POOL=101300, 0, 0 \$END \$LIST POOL=101400, 9, 2, 1, 1 \$END * HS #2 - CYLINDER WALL BETWEEN E1. 29'6" AND 112'0" \$LIST POOL=102001, 100, 7, 0, 0, 0, 0, 38120 \$END \$LIST POOL=102101, 5, 0.00075, 3, 0.02158, 10, 0.06360, 3, 0.02193, 3, 0.02193, 10, 0.06360, 20, 0.14694, 37, 0.917761, 21, 4.35526 \$END \$LIST POOL=102201, 4, 1, 5, 2, 2, 2, \$END \$LIST POOL=102300, 0, 0 \$END \$LIST POOL=102400, 9, 2, 1, 1 \$END * HS #3 - CYLINDER WALL BETWEEN E1. 15'C" AND E1. 29'6" \$LIST POOL=103001, 100, 7, 0, 0, 0, 0, 6667.38 \$END \$LIST POOL=103101, 5, 0.00075, 3, 0.02158, 3, 0.02193, 10, 0.06360, 20, 0.14694, 37, 0.917761, 21, 4.35526 \$END \$LIST POOL=103201, 4, 1, 5, 2, 2, 2, 2 \$END \$LIST POOL=103300, 0, 0 \$END \$LIST POOL=103400, 9, 2, 0, 2 \$END * HS #4 - BASEMAT (OTHER THAN REACTOR BASEMAT) \$LIST POOL=104001, 53, 5, 0, 0, 0, 0, 12800 \$END \$LIST POOL=104101, 3, 0.00067, 7, 20, 1.52698, 2, 1.54781, 20, 11.02150 \$END \$LIST POOL=104201, 4, 2, 2, 1, 2 \$END \$LIST POOL=104300, 0, 0 \$END \$LIST POOL=104400, 3, 3, 0, 3 \$END * HS #5 - REACTOR BASEMAT & S.G. PEDESTALS \$LIST POOL=105001, 70, 4, 0, 0, 0, 0, 1644 \$END \$LIST POOL=105101, 4, 0.00158, 10, 0.1, 30, 2.00, 25, 8.43092 \$END \$LIST POOL=105201, 4, 2, 2, 2 \$END \$LIST POOL=105300, 0, 0 \$END \$LIST POOL=105400, 3, 3, 0, 3 \$END * HS #6 - REACTOR CAVITY WALLS BELOW E1. 15'0" \$LIST POOL=106001, 93, 5, 1, 11.75, 0, 0, 21.5 \$END \$LIST POOL=106001, 5, 11.75192, 7, 11.77292, 30, 13.29923, 30, 19.29923, 20, 25.25192 \$END \$LIST POOL=106201, 4, 2, 2, 2, 2 \$END \$LIST POOL=106300, 0, 0 \$END \$LIST POOL=106400, 3, 3, 0, 3 \$END

Subject CONTAINMENT P/T DESIGN BASIS MSLB

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Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B

Sheet No. B- 33

* HS #7 - REACTOR CAVITY WALLS ABOVE E1. 15'0"	NAME AND POST OF THE OWNER, OF THE OWNER, WHEN PERSONS ASSESSED.	
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* HS #7 - REACTOR CAVITY WALLS AROVE ET 15:0"		
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\$LIST POOL=107001, 68, 5, 0, 0, 0, 0, 2810 \$END		
\$LIST POOL=107101, 5, 0.00192, 7, 0.02292.		1
15, 0.40192, 20, 2.00, 20, 4.00192 \$END		1
\$LIST POOL=107201, 4, 2, 2, 2, \$END		
\$LIST POOL=107300, 0, 0 \$END		
\$LIST POOL=107400, 9, 2, 0, 2 \$END		
* HS #8 - LINED REFUELING CANAL WALLS \$LIST POOL=108001, 86, 6, 0, 0, 0, 9200 \$END		
\$LIST POOL=108101, 5, 0,01563, 20, 0,1		
\$LIST POOL=108101, 5, 0.01563, 20, 0.1, 15, 0.41563, 20, 2.00, 20, 4.01563, 5, 4.01755 \$END		
20, 4.01563, 5, 4.01755 \$END		
\$LIST POOL=108201, 3, 2, 2, 2, 4 \$END \$LIST POOL=108300, 0, 0 \$END		
\$LIST POOL=108400, 9, 2, 9, 2 \$END		1
* HS #9 - S.G. CMPRTMNT WALLS, UNLINED REFL CNL WALLS/OTH INT WALLS		
\$LIST POOL=109001, 78, 4, 0, 0, 0, 0, 41976 \$END		
\$LIST POOL=109101, 5, 0.00192, 10, 0.04233, 12, 0.1, 50, 1.71876 \$END		
\$LIST POOL=109201, 4, 2, 2, 2 \$END		
\$LIST POOL=109300, 0, 0 \$END		
\$LIST POOL=109400, 9, 2, 0, 2 \$END		
* HS #10 - FLOOR SLABS (OTHER THAN BASEMATS) \$LIST POOL=110001, 67, 6, 0, 0, 0, 17474 \$END		1
\$LIST POOL=110101, 3, 0.00014, 5, 0.005348,		
20, 0.105348, 15, 0.505348,		
20, 1.505348, 3, 1.506015 \$END		
\$LIST POOL=110201, 4, 1, 2, 2, 2, 4 \$END \$LIST POOL=110300, 0, 0 \$END		
\$LIST POOL=110400, 9, 2, 9, 2 \$END		
* HS #11 - LIFTING DEVICES (EXCEPT STAINLESS STEEL PARTS)		
X11X1 POOL = 111001 17 2 0 0 0 67296 CEND		
\$LIST POOL=111001, 17, 2, 0, 0, 0, 57286 \$END		
\$LIST POOL=111101, 6, 0.00125, 10, 0.042917 \$END		
\$LIST POOL=111101, 6, 0.00125, 10, 0.042917 \$END \$LIST POOL=111201, 4, 1 \$END \$LIST POOL=111300, 0, 0 \$END		
\$LIST POOL=111101, 6, 0.00125, 10, 0.042917 \$END \$LIST POOL=111201, 4, 1 \$END \$LIST POOL=111300, 0, 0 \$END \$LIST POOL=111400, 9, 2, 0, 2 \$END		
\$LIST POOL=111101, 6, 0.00125, 10, 0.042917 \$END \$LIST POOL=111201, 4, 1 \$END \$LIST POOL=111300, 0, 0 \$END \$LIST POOL=111400, 9, 2, 0, 2 \$END * HS #12 - MISCELLANEOUS CARBON STEEL - THICKNESS > 2.50 INCHES		
\$LIST POOL=111101, 6, 0.00125, 10, 0.042917 \$END \$LIST POOL=111201, 4, 1 \$END \$LIST POOL=111300, 0, 0 \$END \$LIST POOL=111400, 9, 2, 0, 2 \$END * HS #12 - MISCELLANEOUS CARBON STEEL - THICKNESS > 2.50 INCHES \$LIST POOL=112001, 64, 4, 0, 0, 0, 0, 516 \$END		
\$LIST POOL=111101, 6, 0.00125, 10, 0.042917 \$END \$LIST POOL=111201, 4, 1 \$END \$LIST POOL=111300, 0, 0 \$END \$LIST POOL=111400, 9, 2, 0, 2 \$END * HS #12 - MISCELLANEOUS CARBON STEEL - THICKNESS > 2.50 INCHES \$LIST POOL=112001, 64, 4, 0, 0, 0, 0, 516 \$END \$LIST POOL=112101, 6, 0.0005, 17, 0.084, 15, 0.20, 25, 0.310849 \$END		
\$LIST POOL=111101, 6, 0.00125, 10, 0.042917 \$END \$LIST POOL=111201, 4, 1 \$END \$LIST POOL=111300, 0, 0 \$END \$LIST POOL=111400, 9, 2, 0, 2 \$END * HS #12 - MISCELLANEOUS CARBON STEEL - THICKNESS > 2.50 INCHES \$LIST POOL=112001, 64, 4, 0, 0, 0, 0, 516 \$END \$LIST POOL=112101, 6, 0.0005, 17, 0.084, 15, 0.20, 25, 0.310849 \$END \$LIST POOL=112201, 4, 1, 1, 1 \$END		
\$LIST POOL=111101, 6, 0.00125, 10, 0.042917 \$END \$LIST POOL=111201, 4, 1 \$END \$LIST POOL=111300, 0, 0 \$END \$LIST POOL=111400, 9, 2, 0, 2 \$END * HS #12 - MISCELLANEOUS CARBON STEEL - THICKNESS > 2.50 INCHES \$LIST POOL=112001, 64, 4, 0, 0, 0, 0, 516 \$END \$LIST POOL=112101, 6, 0.0005, 17, 0.084, 15, 0.20, 25, 0.310849 \$END \$LIST POOL=112201, 4, 1, 1, 1 \$END \$LIST POOL=112300, 0, 0 \$END		
\$LIST POOL=111101, 6, 0.00125, 10, 0.042917 \$END \$LIST POOL=111201, 4, 1 \$END \$LIST POOL=111300, 0, 0 \$END \$LIST POOL=111400, 9, 2, 0, 2 \$END * HS #12 - MISCELLANEOUS CARBON STEEL - THICKNESS > 2.50 INCHES \$LIST POOL=112001, 64, 4, 0, 0, 0, 0, 516 \$END \$LIST POOL=112101, 6, 0.0005, 17, 0.084, 15, 0.20, 25, 0.310849 \$END \$LIST POOL=112201, 4, 1, 1, 1 \$END		

ICCN NO./ PAGE 35 OF 52 PRELIM. CCN NO. N-2

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B CCN NO. CCN - 2

A	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	T
2	ALLEN EVINAY	01/27/95	PAUL BARBOUR	02/14/95						
* \$1 \$1 \$1 \$1 \$1 \$1 \$1 \$1 \$1 \$1 \$1 \$1 \$1	LIST POOL = 113 LIST POOL = 113 LIST POOL = 113 LIST POOL = 113 LIST POOL = 114 LIST POOL = 115 LIST POOL = 116 LIST POOL = 116 LIST POOL = 116 LIST POOL = 117 LIST POOL = 118 LIST POOL = 118 LIST POOL = 119 LIST POOL = 11	201, 4, 300, 0, 400, 9, ELLANEO 6001, 17 6101, 6, 6201, 4, 6300, 0, 6400, 9, ELLANEO 7001, 16	1 \$END 0 \$END 2, 0, 2 \$US CARBON , 2, 0, 0, 0.000674, 1 \$END 0 \$END 2, 0, 2 \$US CARBON , 2, 0, 0, 0.000606, 1 \$END 2, 0, 2 \$EQUIPMENT 1, 0, 0, 0.0054 \$E \$EQUIPMENT 1, 0, 0, 0.0054 \$E \$END 0 \$END 2, 0, 2 \$US STAINLE 1, 0, 0, 0.01747 \$END 0 \$END 2, 0, 2 \$US STAINLE 1, 0, 0, 0.01747 \$END 0 \$END 2, 0, 2 \$UELING CAN , 4, 0, 0, 0, 0.00192, 0.40192, 2, 2, 2 \$UELING CAN , 4, 0, 0, 0, 0.00192, 0.40192, 2, 2, 2 \$UELING CAN , 4, 0, 0, 0, 0.00192, 0.40192, 2, 2, 2 \$UELING CAN , 4, 0, 0, 0, 0.00192, 0.40192, 2, 2, 2 \$UELING CAN , 4, 0, 0, 0, 0.00192, 0.40192, 2, 2, 2 \$UELING CAN , 4, 0, 0, 0, 0.00192, 0.40192, 2, 2, 2 \$UELING CAN , 4, 0, 0, 0, 0.00192, 0.40192, 2, 2, 2 \$UELING CAN , 4, 0, 0, 0, 0.00192, 0.40192, 2, 2, 2 \$UELING CAN , 4, 0, 0, 0, 0.00192, 0.40192, 2, 2, 2 \$UELING CAN , 4, 0, 0, 0, 0.00192, 0.40192, 2, 2, 2 \$UELING CAN , 4, 0, 0, 0, 0.00192, 0.40192, 2, 2, 2 \$UELING CAN , 5, 7, 0, 0.00075, 0.70944, 4.87885 \$1, 5, 2, 0 \$UELING CAN , 5, 2, 0, 5 \$UELING CAN , 6, 5, 6, 7, 0, 0, 0.00192, 0.40192, 2, 2, 2 \$UELING CAN , 7, 0, 0, 0, 0.00192, 0.40192, 2, 2, 2 \$UELING CAN , 6, 7, 0, 0, 0, 0.00192, 0.40192, 2, 2, 2 \$UELING CAN , 7, 0, 0, 0, 0.00192, 0.40192, 2, 2, 2 \$UELING CAN , 7, 0, 0, 0, 0.00192, 0.40192, 2, 2, 2 \$UELING CAN , 7, 0, 0, 0, 0.00192, 0.40192, 2, 2, 2 \$UELING CAN , 7, 0, 0, 0, 0.00192, 0.40192, 2, 2, 2 \$UELING CAN , 7, 0, 0, 0, 0.00192, 0.40192, 2, 2, 2 \$UELING CAN , 7, 0, 0, 0, 0, 0, 0, 0, 0, 0, 0, 0, 0, 0,	END STEEL: 0 0, 0, 6 13, 0.0 END STEEL: 1 0, 0, 9 10, 0.0 END SS STEEL 0, 0, 2 \$END END AL WALLS 0, 0, 3 7, 0.02 2 20, 2.00 END #3: SE0 #3: SE0 20, 0 END 20, 0 END 2, 2, 2	0.50"< 64693 5 938607 HICKNE 98913.6 912833 644.5 24048 5 644.5 700 \$8 92, 9192 \$8 0.66742 0.79278	THICKNESS<1. SEND SEND SEND SEND SEND WITH STIFFE S8 SEND	NERS 66777,			

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Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B CCN CONVERSION CCN NO. CCN - 2

\$LIST POOL=120201, 4, 1 \$END \$LIST POOL=120400, 9, 2, 0, 2 \$END \$LIST POOL=410001, 25, 54, 0.8, 30, 10, 54, 0.1, 20, 0.0174, 0.0103 \$END \$LIST POOL=500000 \$END	\$LIST POOL=120201, 4, 1 \$END \$LIST POOL=120300, 0, 0 \$END \$LIST POOL=120400, 9, 2, 0, 2 \$END \$LIST POOL=410001, 25, 54, 0.8, 30, 10, 54, 0.1, 20, 0.0174, 0.0103 \$END
\$LIST POOL=120201, 4, 1 \$END \$LIST POOL=120300, 0, 0 \$END \$LIST POOL=120400, 9, 2, 0, 2 \$END \$LIST POOL=410001, 25, 54, 0.8, 30, 10, 54, 0.1, 20, 0.0174, 0.0103 \$END	\$LIST POOL=120201, 4, 1 \$END \$LIST POOL=120300, 0, 0 \$END \$LIST POOL=120400, 9, 2, 0, 2 \$END \$LIST POOL=410001, 25, 54, 0.8, 30, 10, 54, 0.1, 20, 0.0174, 0.0103 \$END

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Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B CCN CONVERSION CCN NO. CCN - 2

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	T
A	ALLEN EVINAY	01/27/95	PAUL BARBOUR	02/14/95				1712	DAIL	١.
						The state of the s			-	۱ ۱

TSMSLB CPi = 16.2 psia 9.2

Subject CONTAINMENTER DESIGN BASIC MET D

*DBMSLB 102%P, Pi=16.2, EV=0%, CT=1, TC=50, LOP=0, CS=1600, N-4080-027-SUP-B \$LIST POOL=0,0,1,0,1 \$END \$LIST POOL=1,1E5,16.2,2.305E6,120,0.6,20,582.945,1,1,0.00,14.7,0.5 \$END

All other input data is identical to the DBMSLB input data.

PRELIM. CON NO.

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CCN CONVERSION 2

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B CCN NO. CCN - 2

Subject CONTAINMENT P/T DESIGN BASIS MSLB

Sheet No. B-37

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	
A	ALLEN EVINAY	01/27/95	PAUL BARBOUR	02/14/95						FY.
	Value of the same of									

10.0 SELECTED OUTPUT DATA

The tabulated data presented in Sections 10.1 and 10.2 consists of partial output of the COPATTA calculation made for this analysis.

10.1

Table for Figures 2-1, 2-2 and 2-4

		CONTAINMENT		
TIME	PRESSURE	VAPOR TEMPERATURE	SUMP TEMPERATURE	HEAT SINK 1 LEFT BOUNDARY
(SEC)	(PSIG)	(F)	(F)	(F)
0	0.0	120.0	120.0	118.4
5	13.7	289.3	178.8	136.0
10	23.3	349.8	204.3	153.4
15	29.8	378.0	218.9	166.6
20	34.8	394.0	228.4	178.5
25	38.8	404.5	235.4	188.0
30	42.4	412.1	240.8	196.2
35	45.7	417.7	245.1	203.4
40	48.6	422.1	248.8	210.1
45	51.2	425.3	251.9	216.7
50	53.5	427.7	254.7	222.6
55	54.9	418.4	257.2	227.7
60	56.3	409.6	259.3	232.4
62	56.6	406.0	260.1	n/a
65	56.1	398.6	261.2	235.4
70	54.6	385.3	262.6	236.9

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CCN CONVERSION

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE
A	ALLEN EVINAY	01/27/95	PAUL BARBOUR	02/14/95				THE REST CONTRACT OF SIX NAME AND ADDRESS OF SIX NAME	

		CONTAINMENT		
TIME	PRESSURE	VAPOR TEMPERATURE	SUMP TEMPERATURE	HEAT SINK 1 LEFT BOUNDARY
(SEC)	(PSIG)	(F)	(F)	(F)
75	53.1	372.0	263.6	238.1
80	51.6	359.0	264.3	239.0
85	50.2	346.3	264.8	239.9
90	49.0	333.9	265.2	240.6
95	47.7	321.5	265.5	241.1
100	46.5	309.2	265.7	241.5
105	45.4	297.8	265.9	n/a
110	44.2	285.8	265.9	n/a
120	43.3	267.0	256.0	n/a
200	37.6	259.7	264.7	243.6
300	33.7	253.3	262.1	241.0
400	30.9	248.1	259.4	238.0
600	26.7	239.8	254.2	232.0
800	23.5	232.7	248.9	225.9
1000	20.8	226.1	243.6	220.3
2000	13.7	204.7	224.1	204.6
4000	6.2	169.4	199.8	172.3
6000	3.0	145.1	182.9	157.8
8000	1.8	132.3	170.7	148.3
9000	1.50	128.6	165.9	144.8
10000	1.25	125.8	161.7	141.9

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CON CONVERSION

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B CCN NO. CCN -

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE
1	ALLEN EVINAY	01/27/95	PAUL BARBOUR	02/14/95					

10.2 (continued)

Table for FIGURE 2-5

Integrated Energy Transferred from the Containment Vapor Region by one Train of Air Coolers, 2ECUs and one Train of Containment Spray v.s. Time

		INTEGRATED	ENERGY			
TIME	STEAM	AIR	VAPOR	SUMP	TOTAL	HEAT SINKS
SEC	BTU	ВТИ	BTU	BTU	BTU	BTU
1	3.23e+07	1.71e+07	4.93e+07	1.35e+04	4.93e+07	2.22e+04
3	4.26e+07	1.78e+07	6.03e+07	3.40e+04	6.04e+07	2.63e+05
5	6.17e+07	1.88e+07	8.05e+07	1.05e+05	8.06e+07	7.28e+05
10	1.02e+08	2.04e+07	1.23e+08	4.71e+05	1.23e+08	2.79e+06
15	1.31e+08	2.11e+07	1.52e+08	1.05e+06	1.53e+08	5.73e+06
20	1.53e+08	2.15e+07	1.75e+08	1.77e+06	1.76e+08	9.19e+06
25	1.72e+08	2.17e+07	1.94e+08	2.58e+06	1.96e+08	1.29e+07
30	1.88e+08	2.19e+07	2.10e+08	3.44e+06	2.14e+08	1.67€+07
35	2.04e+08	2.21e+07	2.26e+08	4.31e+06	2.30e+08	2.05e+07
40	2.17e+08	2.22e+07	2.39e+08	5.19e+06	2.45e+08	2.42e+07
45	2.30e+08	2.23e+07	2.52e+08	6.08e+06	2.58e+08	2.80e+07
50	2.41e+08	2.23e+07	2.63e+08	6.97e+06	2.70e+08	3.30e+07
55	2.51e+08	2.20e+07	2.73e+08	7.88e+06	2.81e+08	3.52e+07
60	2.61e+08	2.19e+07	2.83e+08	8.77e+06	2.92e+08	3.86e+07
65	2.65e+08	2.16e+07	2.86e+08	9.63e+06	2.96e+08	4.19e+07
70	2.61e+08	2.12e+07	2.83e+08	1.04e+07	2.93e+08	4.49e+07
75	2.58e+08	2.09e+07	2.79e+08	1.12e+07	2.90e+08	4.76e+07
100	2.46e+08	1.93e+07	2.65e+08	1.40e+07	2.79e+08	5.85e+07
200	2.12e+08	1.81e+07	2.31e+08	2.54e+07	2.56e+08	8.11e+07

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Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-927 Supplement B CCN CONVERSION CCN NO. CCN - 2

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	_
A	ALLEN EVINAY	01/27/95	PAUL BARBOUR	02/14/95				-		Name of the last

		INTEGRATED	ENERGY	Fig 2-5		
TIME	STEAM	AIR	VAPOR	SUMP	TOTAL	HEAT SINKS
SEC	вти	BTU	BTU	ВТИ	вти	BTU
300	1.91e+08	1.79e+07	2.09e+08	3.47e+07	2.44e+08	9.30e+07
400	1.76e+08	1.78e+07	1.93e+08	4.25e+07	2.36e+08	1.00e+08
600	1.52e+08	1.76e+0?	1.70e+08	5.61e+07	2.26e+08	1.10e+08
800	1.34e+08	1.74e+07	1.52e+08	6.79e+07	2.20e+08	1.16e+08
1000	1.20e+08	1.72e+07	1.37e+08	7.84e+07	2.15e+08	1.20e+08
2000	8.02e+07	1.67e+07	9.69e+07	1.21e+08	2.18e+08	1.21e+08
4000	3.87e+07	1.58e+07	5.45e+07	1.86e+08	2.40e+08	1.12e+08
6000	2.21e+07	1.52e+07	3.74e+07	2.36e+08	2.74e+08	1.01e+08
8000	1.60e+07	1.49e+07	3.08e+07	2.79e+08	3.10e+08	8.96e+07
9000	1.43e+07	1.48e+07	2.90e+07	2.99e+08	3.28e+08	8.47e+07
10000	1.29e+07	1.47e+07	2.76e+07	3.19e+08	3.46e+08	8.03e+07

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Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B CCN CONVERSION CCN NO. CCN - 2

Subject CONTAINMENT P/T DESIGN BASIS MSLB Sheet No. B-41

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	
A	ALLEN EVINAY	01/27/95	PAUL BARBOUR	02/14/95						P

FIGURE 2-6 Integrated Heat Transfer of the Air Coolers and Containment Sprays

TIME	INTERGRATED ENERGY CONTAINMENT SPRAYS	INTERGRATED ENERGY AIR COOLERS				
(SEC)	(BTU)	(BTU)				
50		2.31e+03				
55	3.56e+05	1.19e+05				
60	7.03e+05	2.38e+05				
65	1.04e+06	3.57e+05				
70	1.36e+06	4.76e+05				
75	1.67e+06	5.94e+05				
85	2.24e+06	8.24e+05				
100	2.99e+06	1.16e+06				
150	5.28e+06	2.43e+06				
200	6.70e+06	3.24e+06				
250	8.44e+06	4.23e+06				
300	1.01e+07	5.18e+06				
400	1.34e+07	7.02e+06				
500	1.66e+07	9.12e+06				
600	1.95e+07	1.05e+07				
800	2.50e+07	1.36e+07				
1000	3.00e+07	1.66e+07				
2000	5.07e+07	2.88e+07				
3000	6.71e+07	3.81e+07				
4000	8.01e+07	4.49e+07				
6000	9.87e+07	5.34e+07				
8000	1.11e+08	5.81e+07				
0,000	1.20e+08	6.11e+07				

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Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B

Su	bject	CONTAINM	ENT P/T	DESIGN BAS	SIS MSLB				Sheet	No. P	3- 42
F	REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRF	DATE	-

I I EN EVINAY	01 107 105					DATE	4
ELLI ETINAT	01/27/95	PAUL BARBOUR	02/14/95				N. MCATTE
							50

FIGURE 2-7

Rate of Energy Transfer from the Vapor Region by a Single Train of Emergency Cooling Units (2ECUs) and by a Single Train of Containment Sprays vs Time

TIME	ENERGY REMOVAL RATE BY CONTAINMENT SPRAYS	TIME	ENERGY REMOVAL RATE BY CONTAINMENT AIR COOLERS
secs	(btu/hr)xE6	secs	(btu/hr)xE6
51.5	258.1	50	82.7
60.0	246.0	60	85.4
99.5	167.3	100	78.6
200	126.9	200	72.1
500	110.3	500	61.8
975	85.0	1000	50.9
2750	55.7	2500	33.7
5000	33.1	5000	15.0
7750	19.6	7500	7.5
10000	15.5	10000	4.4

ICCN NO./ PRELIM. CCN NO.

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CCN CONVERSION CCN NO. CCN - 2

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027 Supplement B

IRE

PAUL BARBOUR

CONTAINMENT P/T DESIGN BASIS MSLB Subject DATE

01/27/95

 Sneet	NO	B- 43
IRE	DATE	
		1,0
		- 69

APPENDIX A (COPATTA Code I/O File)

The COPATTA Code input files are presented in Section 9 of this calculation.

DATE

02/14/95

REV

ORIGINATOR

The COPATTA Code output files are included on Microfiche. The output file name and date are as follows:

FICHE TITLE :

ORIGINATOR

ALLEN EVINAY

DBMSLB J5284 18-Jan-95

JOB TITLE

REV

*DBMSLB 102%P, CPi=14.7, EVAP=0%, CT=1, LOP=0, CS=1600,

N-4080-027-SUP-B

RUN DATE

20-Dec-94

LAST SHEET :

:

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FICHE TITLE :

TSMSLB J5303 18-Jan-95

JOB TITLE

*TSMSLB 102%P, CPi=16.2, EVAP=0%, CT=1, LOP=0, CS=1600.

N-4080-027-SUP-B

RUN DATE

28-Dec-94

LAST SHEET :

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CALCULATION SHEET

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Project or DCP/MMP SONGS Units 2 & 3 Calc. No. N-4080-027

CCN CONVERSION: CCN NO. CCN - 2

Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

Sheet No. 6

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	T o
0	S. Oliver	12/30/93	J. Elliott	1/4/94		CONTRACTOR OF THE PARTY OF THE		THE RESERVE AND ADDRESS OF THE PERSON NAMED IN COLUMN 2 IN COLUMN	-	E
	A.EVINAY	3/14/95	P. BARBOUR	3/14/95					+	I V

THIS SECTION REPLACED BY SECTION 2 IN SUPPLEMENT B

RESULTS/CONCLUSIONS AND RECOMMENDATIONS

2.1 RESULTS/CONCLUSIONS

Figure 24 presents the sump and vapor pressures versus time for the DBA MSLB. The plots in Figure 2-1 are generated using the data presented in Section 10.1.

Figure 2-2 presents the containment gauge pressure versus time for the DBA MSLB. The plot in Figure 2-2 is generated using the data presented in Section 10.1.

Figure 2-3 presents the condensing heat transfer coefficient used by the COPATTA Code versus time for the DBA MSLB. The plot in Figure 2-3 is generated using the data presented in Section 10.1.

Figure 2-4 presents the inside surface temperature of heat sink 1 (reactor building dome) to represent the temperature of the containment structure. The plot in Figure 2-4 is generated using the data presented in Section 10.1.

Figure 2-5 presents the instantaneous energy vs. time data used by COPATTA to determine heat transfer in the DBA MSLB. The plots by Figure 2-5 are generated using the data presented in Section 10.2. Included are:

VAPOR ENERGY: Instantaneous steam + air energy.

SUMP ENERGY:

Instantaneous energy of sump water.

TOTAL ENERGY: Instantaneous energy inventory.

HEAT SINKS:

Instantaneous energy stored in structures.

Figure 2-6 presents the integrated heat transfer of the air coolers and containment sprays. The plots presented in figure 2-6 are generated using the data in Section 10.2. Included are:

AIR COOLERS

Integrated energy removed by emergency fan coolers.

CONT. SPRAY:

Integrated energy transferred to sump by sprays.

The following table presents the accident chronology for the analysis.

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Project or DCP/MMP SONGS Units 2 & 3 Calc. No. N-4080-027

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Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

Sheet No. _7

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	5.25	MARIN
0	S. Oliver	12/30/93	J. Elliott	1/4/94	-		DAIL	INE	DATE	E
S. O. P. S. Coner.	A. EVINAY	3/14/95	P. BARLOUR	3/14/94					+	V 11

THIS TEXT AND TABLE REPLACED BY TEXT IN SEC. 2 & TABLES 2-1 \$ 2-2 IN SUPPLEMENT B

TIME (seconds)	EVENT
0.0	Break occurs
15	Emergency fan coolers start (at full capacity)
50	Containment spray nozzles at full discharge flow
50 0	Peak containment temperature of 421 °F
62.3	Peak containment pressure of \$8.5 psig
74_08	End of Blowdown

Note that although the peak vapor temperature of 421 °F is greater than the 300 °F design temperature, the duration of the event is sufficiently small to prevent heating of the containment structural materials beyond the design limits. As indicated by Figure 2-4, the 241 °F peak surface temperature of the containment liner remains well below 300 °F. Because the liner inside surface (actually a layer of organic paint) remains below 300 °F, the containment structure will not exceed design temperatures.

As can be seen from Figures 2-2 and 24, the peak pressure (58.5 psig) is below the design pressure of 60 psig and the peak temperature of the containment structure (241 °F) is below the design temperature of 300 °P. Therefore, General Design Criteria 16 and 50 (See Section 1.2) are met. The gauge pressure with respect to the outside atmosphere at 10,000 seconds is less than 3.0 psig. The pressure remaining after 24 hours is therefore expected to be only a small fraction of the 60 psig design pressure; therefore, the requirements of General Design Criterion 38 (See Section 1.2) are met.

CALCULATION SHEET

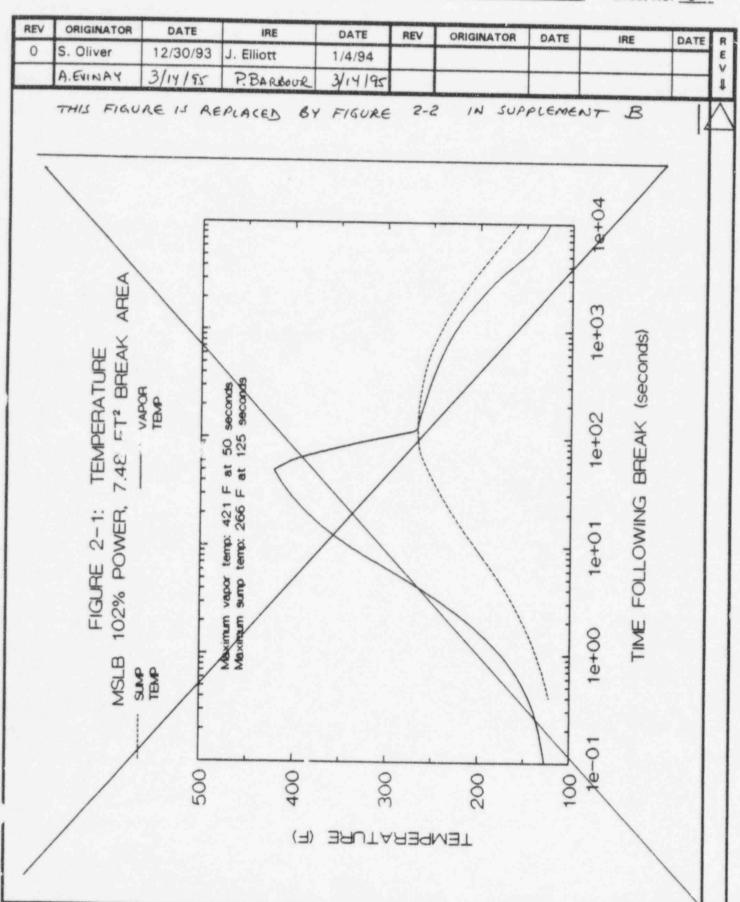
ICCN NO./ PRELIM. CCN NO. N-2 PAGE 470F 52

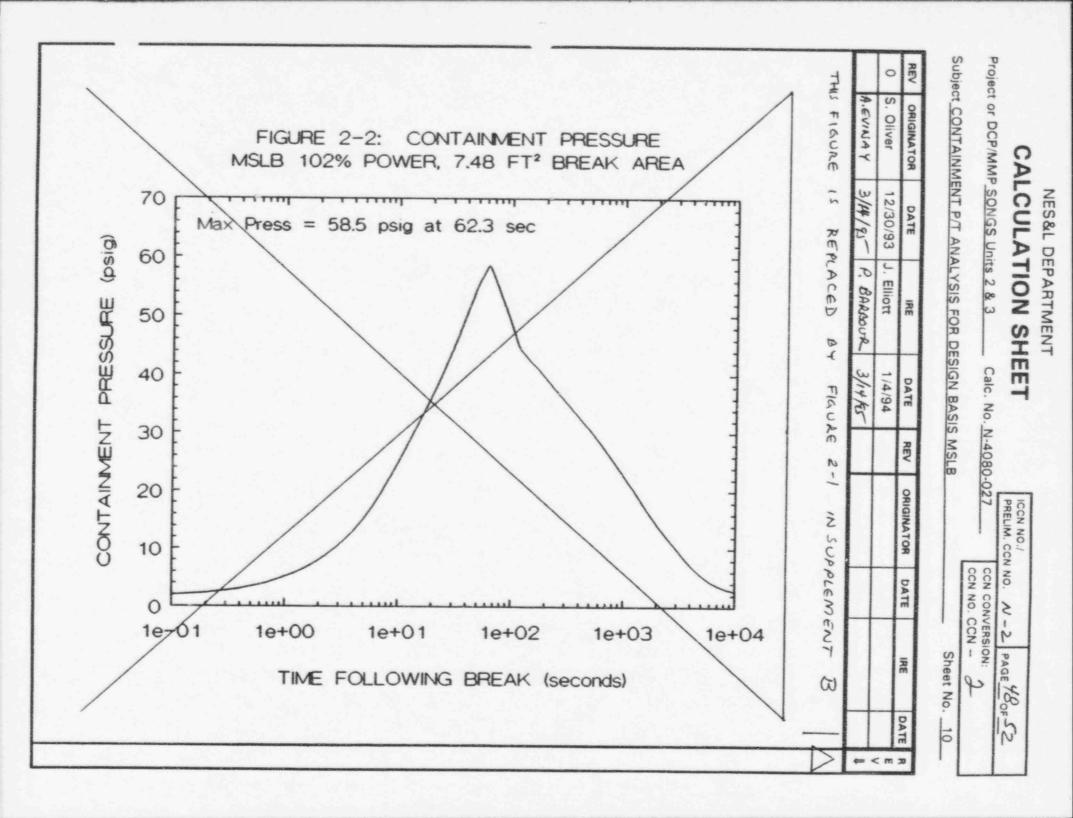
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Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

Sheet No. 9





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Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

Sheet No.

	1.	No. of Street, or other Persons	OREV
FIGURE 2-3: CONDENSING HTC MSLB 102% POWER, 7.48 FT ² BREAK AREA	THU FIGURE	A.EVINAY	S. Oliver
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135 111.9 BYU/hr-ft²-F at 64 s (L) 120 - 105 -	REPLACED	P. BARBO VA	J. Elliott
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Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

FIGURE 2-4: LINER PLATE SURFACE TEMP. MSLB 102% POWER, 7,48 FT2 BREAK AREA HEAT SINK 1 REFT BOUND 12/30/93 DATE 300 Maximum liner plate surface temperature: 241/F at 150 seconds BARROW Elliott RE 260 E 34 TEMPERATURE TRURE DATE 1/4/94 220 REV N 180 V ORIGINATOR 140 JUPPLEMEN DATE 100 1e+00 1e+01 1e+03 1e+02 RE TIME FOLLOWING BREAK (seconds) D DATE

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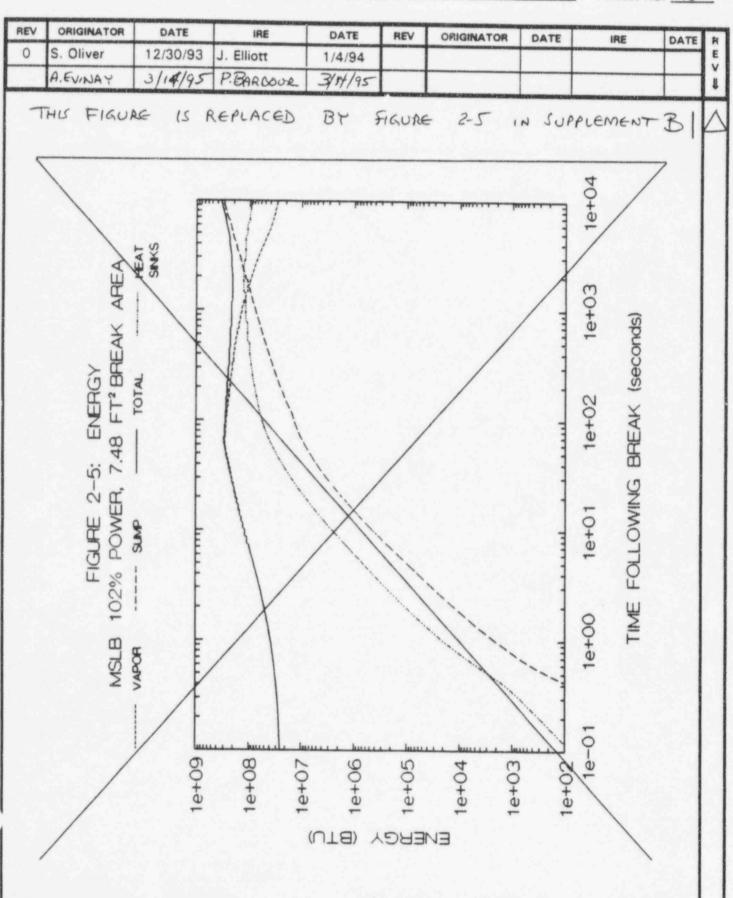
ICCN NO./ PAGE 5/ OF 52 PRELIM. CON NO. N-Z

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Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

Sheet No. 13



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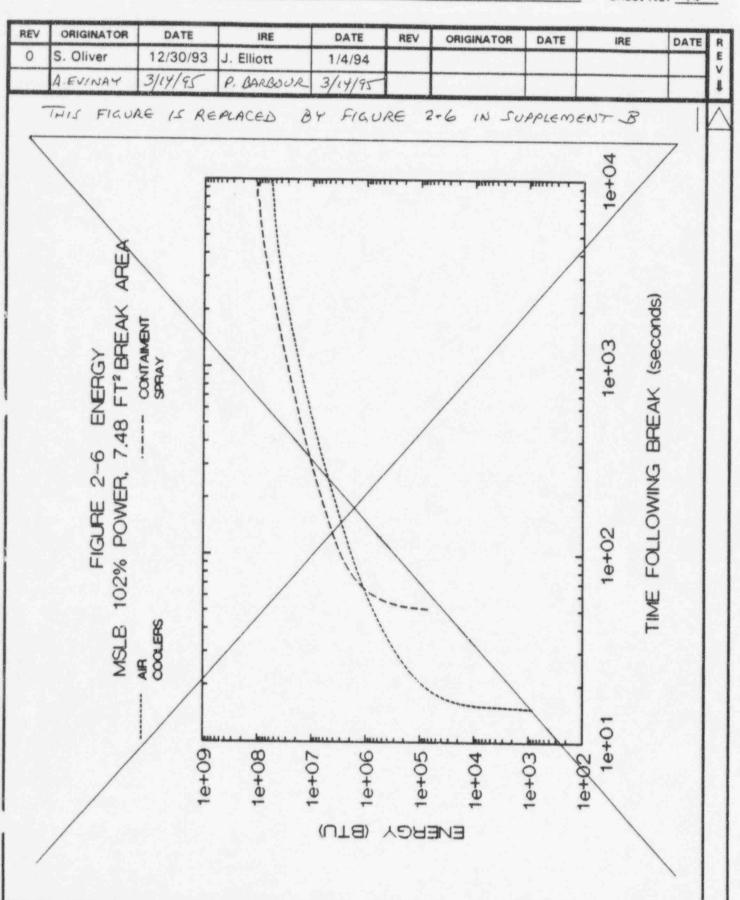
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Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

Sheet No. 14



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Add Supplement A to the base calculation.

Supplement A provides a new Analysis of Record for the Containment Building pressure and temperature reaponse to the Design Basis MSLB event specifically applicable to the evaluation of the environmental qualification of in-containment equipment, important to safety, that must function during and/or following a design basis accident. The analysis results are applicable only to equipment qualification because of the inclusion of 8% condensate revaporization which slightly lowers the calculated peak containment pressure and vapor temperature below the values calculated to support containment structural design, and reported in Section 6.2 of the UFSAR.

2. OTHER AFFECTED DOCUMENTS (CHECK AS AP See Calc Cross Inc.	PLICABLE FOR CON ONLY);	030002-02, 93030003-02, and 93030004-02 ARE IDENTIFIED ON ATTACHED FORM 26-503.	Rev.
3. APPROVAL:		DISCIPLINE/ESC: NUCLEAR SAFETY	ANALYSIS
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PAUL BARBOUR IRE (Print name/initial) PAX	51379	NES&L DM (Signature)	OTHER (Signature)
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PAGE 2 OF 4/

A 40 Containment P/T Design Basis MSLB for Equipment Qualification - SUPPLEMENT A Sheet All system Number/Primary Station System Designator 1301 / ABB SONGS Unit 263 Q-Class II sech. Spec. Affecting? No Q YES, Section No. N/A Equipment Tag No. N/A CONTROLLED COMPUTER PROGRAM DATABASE IN ACCORDANCE WITH NES&L 41-5-1 NACCORDANCE WITH NES&L 41-5-1 NE100 (COPATTA) G1-15 RECORDS OF ISSUES REV. DESCRIPTION TOTAL SHTS. (Print name/initial) (Signature) ORIG. ALLEN EVINAY A GS AUTHOR OTHER PAUL BARBOND DATE A 40 IRE DM DATE ORIG. GS Other ORIG. GS Other ORIG. GS Other DATE ORIG. GS OTHER
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is calculation was prepared using Word Perfect 5.1 software as an electric typewriter. The WP5.1 software was not used for any computations of the calculation.

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Calculation No. N-4080-027 - SUPPLEMENT A Sheet No. A2 CCN CONVERSION: CCN NO. CCN

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	Calc/Document No.	Rev. No.	Calc/Document No.	Rev. No.	YES / NO	
Δ	Calculations: N-4080-027 M-0014-009, Supplement A	0 0	UFSAR, Section 3.11.3.1.2 DBD-SO23-TR-EQ	10	Yes Yes	SAR 23-341 NEDOTRAK Log BC-93-079
A) 1 1/4/14	M-0072-036 N-4080-007, incl CCNs 1 & 2	0 2	Calculation M-DSC-243	0	Yes	NEDOTRAK Action 93030001/3 sub#5
			EQDPs M37600 M37601 M37606 M37607 M37608		Yes	NEDOTRAK Log BC-93-079
	Unit 2 Operating Liscense & Technical Specifications Unit 3 Operating License & Technical	Amdt 101	M37609 M37610 M37612 M37615			
	Specifications	Amdt 90	M37618 M37619 M37620 M37621 M37624 M37629 M37631			
	Non-Conformance Reports (NCRs) 93030001 93030002	3 2	M37635 M37636 M37640			
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Du/+/94			EQDPs, cont'd M38290 M38377 M38378 M38379 M38381 M38382 M38383 M38384 M38385 M38773		Yes	NEDOTRAK Log BC-93-079
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1.0 PURPOSE

1.1 TASK DESCRIPTION

The purpose of the Containment P/T Steam Line Break analysis for Equipment Qualification Thermal Analysis performed here is several fold:

- 1.1.1 Determine the containment temperature and pressure response to the Design Basis Main Steam Line Break (MSLB) event for use by the Nuclear Engineering Design Organization (NEDO) Equipment Qualification (EQ) Group as the bounding containment harsh environment resulting from such a MSLB event. The analysis uses the input data from the present analysis of record (AOR) Design Basis MSLB (102% Power MSLB, reference 6.1), modified as necessary to include NUREG-0588 (reference 6.9) methodology applicable to equipment qualification at SONGS and also to conform with the Licensing Organization's interpretation of our licensing basis for P/T Analyses (reference 6.14).
- 1.1.2 Streamline the Containment P/T MSLB Analysis for Equipment Qualification by limiting this analysis to only generating the containment harsh environmental conditions. The Equipment Thermal Lag analysis contained in the present calculation N-4080-004 (reference 6.4) have been largely obsoleted by later analyses (reference 6.10 and 6.11) using more sophisticated equipment modelling.
- 1.1.3 Create a CCN for the existing Containment MSLB P/T Equipment Qualification calculation, N-4080-004 (reference 6.4) to identify Supplement A to N-4080-027 Rev O, as containing the current Design Basis MSLB Containment P/T Response AOR for the in-containment equipment qualification environment .
- 1.1.4 This calculation supplement uses a minimum containment spray flow rate consistent with degraded spray pump performance documented in the calculation M-0014-009 (reference 6.2) and completes NFM action required in the disposition step 2 of NCRs 93030001, 93030002, 93030003 and 93030004.

Bechtel Standard Computer Code NE100, Release G1-15 (COPATTA) (reference 6.5), on the Nuclear Fuels Engineering IBM-RISC workstation system will be used in this calculation to evaluate the containment pressure and temperature transients for the Equipment Qualification Analysis.

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1.2 CRITERIA, CODES and STANDARDS

The criteria, codes and standards applicable to the Containment P/T Analysis for Design Basis MSLB (reference 6.1), are also generally applicable in this analysis. The applicable regulatory design criteria include:

- General Design Criterion (GDC) 16, "Containment Design"
- General Design Criterion (GDC) 38, "Containment Heat Removal"
- General Design Criterion (GDC) 50, "Containment Design Basis".

The applicability of these criteria to peak containment pressure and temperature are described in detail in Reference 6.1.

Additional general criteria applicable to Equipment qualification analysis are contained in

- 10 CFR 50.49, "Environmental qualification of Electric Equipment Important to safety For Nuclear Power Plants"
- NUREG-0588, Revision 1, "Interim Staff Position On Environmental Qualification of Safety-Related Electrical Equipment".

Title 10, CFR 50.49 requires that the time-dependent environmental temperature and pressure at the location of equipment important to safety must be established for the most severe design basis accident during or following which the equipment is required to remain functional.

NUREG-0588 provides methodology applicable to the calculation of post accident environmental conditions and the evaluation of equipment thermal response to the post-accident environment.

The containment design pressure and temperature are 60 psig and 300 °F per the Technical Specifications (references 6.5 and 6.6, Section 5.2.2) respectively.

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2.0 RESULTS/CONCLUSIONS AND RECOMMENDATIONS

2.1 RESULTS/CONCLUSIONS

Figures 2.1 through 2.5 show the analysis results out to 1000 seconds, which is well beyond the time of the affected steam generator dry-out and termination of significant mass and energy release into the containment. At 1000 seconds, the containment temperature and pressure are well below the peak values and decreasing. Section 10 contains tabulated conditions to the end of the transient calculation at 1E+5 seconds.

Figure 2.1 presents the sump and vapor temperatures versus time for the CONTAINMENT P/T DESIGN BASIS MSLB FOR EQUIPMENT QUALIFICATION. The plots in Figure 2.1 are generated using the data presented in Section 10.1.

Figure 2.2 presents the containment gauge pressure versus time for the CONTAINMENT P/T DESIGN BASIS MSLB FOR EQUIPMENT QUALIFICATION. The plot in Figure 2.2 is generated using the data presented in Section 10.1.

Figure 2.3 presents the inside surface temperature of heat sink 1 (reactor building dome, painted steel liner plate) to represent the maximum post-MSLB temperature of the containment structure. The plot in Figure 2.3 is generated using the data presented in Section 10.1.

Figure 2.4 presents the integrated energy transferred from the containment vapor region by one train of air coolers, two Emergency Cooling Units (2ECUs) and one train of containment spray as a function of time. The plots in Figure 2.4 are generated using the data presented in Section 10.2.

Figure 2.5 presents the rate of energy transfer from the vapor region by a single train of emergency cooling units (2ECUs) and by a single train of containment sprays as a function of time. The plots in Figure 2.5 are generated using the data presented in Section 10.2.

Table 1 presents the CONTAINMENT P/T DESIGN BASIS MSLB FOR EQUIPMENT QUALIFICATION accident chronology.

The calculated peak vapor temperature of 407.1 $^{\circ}F$ is greater than the 300 $^{\circ}F$ design temperature, however the duration of the event is sufficiently small enough to prevent heating of the containment structural materials beyond the design limits.

The peak vapor temperature is about $1.5\,^{\circ}F$ greater than the previously identified peak temperature in the prior AOR (N-4080-004, reference 6.4). The increase in the peak temperature is attributed to the reduced ECU heat transfer capacity (M-0072-036, Revision 0, reference 6.12) and the delayed spray start time of 50

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seconds v.s. the prior analysis spray start time of 45 seconds. The containment vapor pressure remains at, or above, $300\,^\circ F$ for about 85 seconds (6 sec to 91 sec) compared to about 79 seconds (6 secs to 85 secs) in the prior analysis in Reference 6.4.

The primary purpose of this calculation is to provide a conservative analysis of the containment pressure-temperature response to the design basis MSLB. The objective is to define containment conditions for post-accident equipment qualification with emphasis on the relatively short time frame when the MSLB harsh environment is more severe than that created by the design basis loss of coolant accident (LOCA). In this regard, an analysis duration of 1000 seconds is more than adequate to simulate the desired post-MSLB harsh environment. However, to provide insight into the longer-term post-MSLB containment environment, the analysis has been extended to 100,000 seconds (~28 hours). The analysis includes containment spray termination at 10,000 seconds, following refueling water storage tank (RWST) inventory depletion. Following termination of containment spray, the vapor temperature rises from 126 °F to about 145 °F due to the reduction in vapor region energy removal rate. The vapor temperature then resumes a slow downward trend continuing to the end of the analysis run time. At the end of the run (1E+5 seconds), the containment pressure and vapor temperature are about 0.6 psig and 132 °F, respectively. The long-term containment cooldown is conservative due to modelling which allows no evaporative or convective heat transfer between the sump water and the vapor region. Thus, in the absence of continued spray, or sump water recirculation, cooling of the containment sump occurs only through heat convection into the flooded lower concrete. In any event, the longer analysis does demonstrate that the longer-term MSLB environment does remain bounded by the design basis LOCA event as provided in N-4080-026 (reference 6.16)

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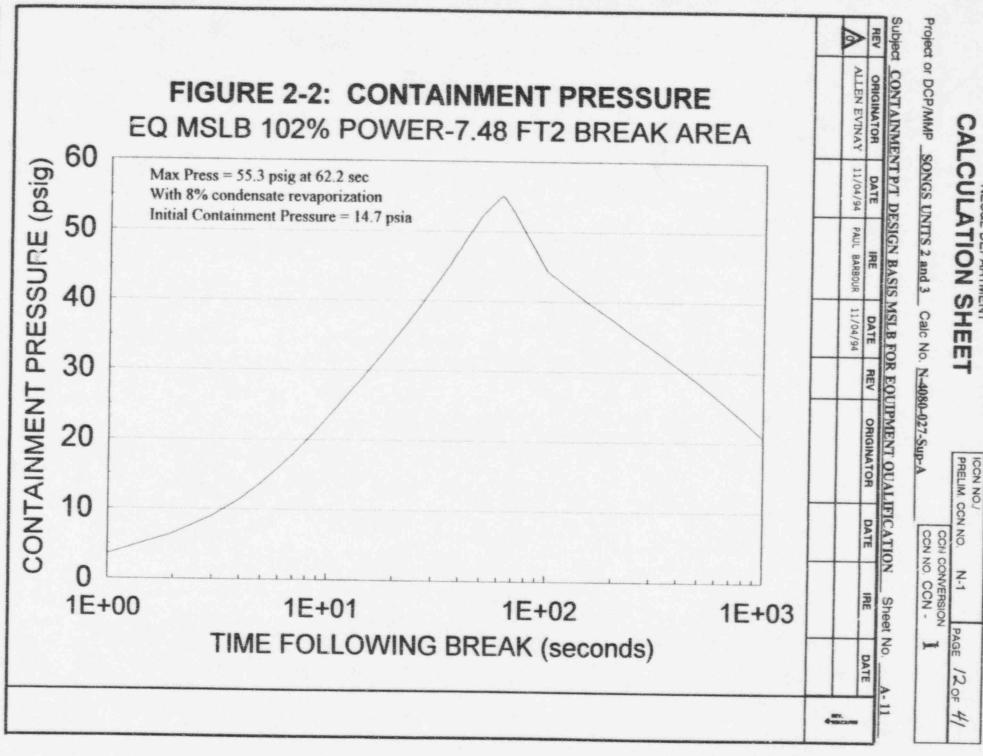
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Table 1

CONTAINMENT P/T DESIGN BASIS MSLB FOR EQUIPMENT QUALIFICATION EVENT CHRONOLOGY

TIME (seconds)	EVENT
0.0	MSLB Occurs
50	Containment Sprays Start (Nozzles at Full Discharge Flow) AND Emergency Fan Coolers Start (Full capacity)
50	Peak Containment Temperature of 407.1 °F reached
62.2	Peak Containment Pressure of 55.3 psig reached
71.08	End of Blowdown (Affected Steam Generator)
175.0	Containment Liner Plate Maximum Temperature of 243.8 °F reached
9000.0	Maximum Tech. Spec. Containment Pressure of 1.499 psig ≤ 1.5 psig reached
10000.0	Containment Spray Flow Terminated Containment Pressure = 1.3 psig Containment Temperature = 125.8 F
100000.0	Containment Pressure = 0.6 psig Containment Vapor Temp = 131.9 °F Containment Sump Temp = 159.8 °F

FIGURE 2-1: TEMPERATURE EQ MSLB 102% POWER-7.48 FT2 BREAK AREA INMENT P/T DESIGN BASIS VAPOR TEMP ---- SUMP TEMP 450 Maximum vapor temp: 407.1 F at 50 seconds Maximum sump temp: 265.4 F at 125 seconds With 8% condensate revaporization 400 Initial Containment Pressure = 14.7 psia TEMPERATURE (F) 350 300 250 ORIGINATOR 200 150 CCN CONVERSION 100 1E+00 1E+01 1E+02 1E+03 TIME FOLLOWING BREAK (seconds)



CALCULATION

Project or DCP/MMP SONGS UNITS 2 and 3

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EQUIPMENT QUALIFICATION

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FIGURE 2-3: LINER PLATE SURFACE TEMP EQ MSLB 102% POWER-7.48 FT2 BREAK AREA HEAT SINK 1 (LEFT BOUND)

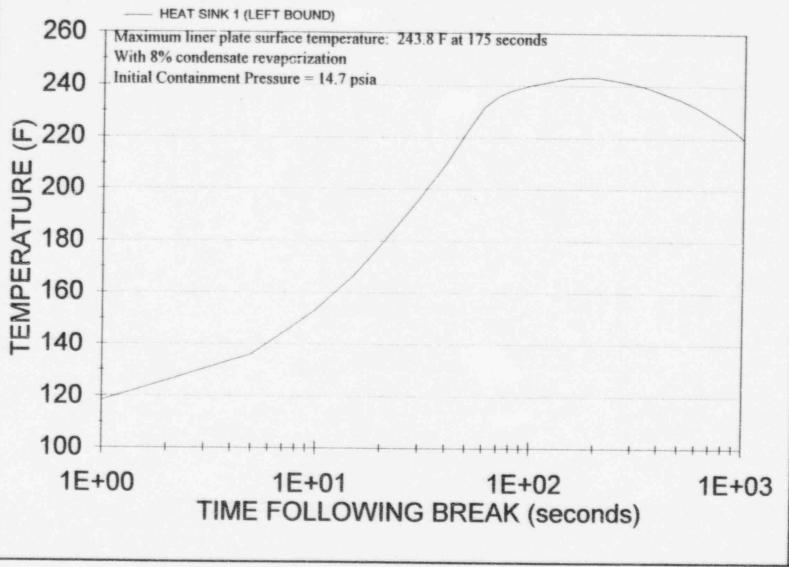


FIGURE 2-4 INTEGRATED ENERGY EQ MSLB 102% POWER-7.48 FT2 BREAK AREA NES&L DEPARTMENT CONTAINMENT SPRAY --- AIR COOLERS 1E8 With 8% condensate revaporzation Initial Containment Pressure = 14.7 Air Coolers on @ 50 seconds 1E7 Sprays on @ 50 seconds **ENERGY (BTU)** 1E6 1E5 1E4 1E+03 CCN CONVERSION 1E+02 1E+02 1E+03 1E+01 TIME FOLLOWING BREAK (seconds)

FIGURE 2-5: VAPOR HEAT REMOVAL RATES EQ MSLB 102% POWER-7.48 FT2 BREAK AREA RATE (1E+06 Btu/hr) 1E+03 AIR COOLERS (2) ---- CONTAINMENT SPRAYS 8% Condensate revaporization Initial containment Pressure = 14.7 psia Air Coolers on @ 50 seconds Sprays on @ 50 seconds 1E+02 HEAT TRANSFER CCN CONVERSION 1E+01 1E+01 1E+02 1E+03 TIME FOLLOWING BREAK (seconds)

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2.2 RECOMMENDATIONS

This Supplement A provides a new analysis of record for the containment pressure and temperature response to the Design Basis MSLB event for Equipment qualification. This analysis replaces the prior containment P/T response analysis contained in N-4080-004 Rev. 1, (Non-Technical CCN to N-4080-004, Rev.1).

Calculation M-DSC-243 (reference 6.10) should be revised to incorporate the new containment temperature response to the Design basis MSLB and to include thermallag analysis for those electrical components modelled in reference 6.4 which are still needed to support the SONGS equipment qualification (NEDOTRAK Action Item Number 93030001/3, sub# 5).

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3.0 ASSUMPTIONS

The assumptions used in this calculation are identical to those used in the Containment P/T Analysis for Design Basis MSLB (reference 6.1), except where noted. Reference 6.1 is the analysis of record (AOR) for the DBA MSLB. The assumptions in reference 6.1 are arranged in groups which parallel the COPATTA Code card series data input. The modifications to reference 6.1 assumptions are listed below.

3.1 CARD SERIES 1

3.1.a ITEM 05: CONTAINMENT INITIAL TEMPERATURE

In both the AOR (reference 6.1) and this analysis, the containment initial temperature was assumed to be 120 °F. This is the SONGS Technical Specification maximum containment average temperature. The containment initial temperature profile at full power operating conditions varies from 140 °F in the upper dome to 80 °F in the basement region. The initiation of MSLB will almost instantaneously homogenize the containment temperature and in less than one half of one second, the containment average initial temperature will be in the vicinity of 120 °F. Henceforth, the use of an initial average temperature of 120 °F is easily justifiable and the results of the calculation are still applicable for the post-accident MSLB containment temperature and pressure profiles.

3.1.b ITEM 11: CONTAINMENT HEAT SINK REVAPORIZATION FRACTION

This MSLB analysis is performed for Equipment Qualification Temperature and Pressure profile generation and therefore credit for revaporization of heat sink condensate will be taken. NUREG-0588 (reference 6.9, Appendix B, Section 1.b) allows for up to 8 percent of the condensate to be transferred to vapor region during the performance equipment qualification analysis. Allowing revaporization of heat sink condensate reduces the containment temperature and pressure relative to zero revaporization.

3.2 CARD SERIES 5

3.2.a ITEM 3: CONTAINMENT EMERGENCY AIR COOLER START TIME

In the AOR (reference 6.1), the containment air cooler start delay time was identified as 15 seconds in the Design Input 4.3.a. In the present analysis the air cooler start time has been increased to 50 seconds to coincide with the containment spray actuation time. The emergency air cooling units have relatively little impact on short-term containment pressure and temperature, and by adding 35 seconds delay to ECU initiation, margin is added to accommodate potential changes in the timing of ECU startup. For example, based on the methodology

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CCN CONVERSION 1

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

CON NO. CON -

EV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	T TOTAL CONTRACTOR
1	ALLEN EVINAY	11/04/94	PAUL BARBOUR	11/04/94						ST.
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cor	ntained in ca	lculati	on N-4080-	003 (ret	ferenc	e 6 15) the	50 secon	nd start	timo	
101	r the ECUs is	equival	ent to ass	uming a	47-se	cond stroke t	ime for	the CCW	block	
Va	lves that sup fecting ECU s	oply cod	oling water	to the	air	coolers, if	all other	er param	eters	
aii	rectifig Eco s	cart tr	me were to	remain	uncha	ngea.				
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ICCN NO./ PRELIM. CON NO.

N-1

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CCN CONVERSION

CON NO. CON -

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

Subject CONTAINMENT P/T DESIGN BASIS MSLB FOR EQUIPMENT QUALIFICATION Sheet No. A-18

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	MILINESIMACION SCHOOL F
A	ALLEN EVINAY	11/04/94	PAUL BARBOUR	11/04/94						
										**

4.0 DESIGN INPUT

The design inputs used in this calculation are identical to those used in the Containment P/T Analysis for Design Basis MSLB (reference 6.1), except where noted. Reference 6.1 is the analysis of record for the DBA MSLB. The design inputs in reference 6.1 are arranged in groups which parallel the COPATTA Code card series data input.

4.1 CARD SERIES O

The last four zero entries on this card are deleted. The G1-15 (RISC) version of COPATTA does not utilize these data entry locations.

4.2 CARD SERIES 1

ITEM 2:

PROBLEM RUN TIME

The problem run time will be set to 1E+5 seconds (~28 hours). The pipe break mass and energy release into the containment provided by the Combustion Engineering (ABB-CE) included on CARD SERIES 301 terminated at 71.08 seconds, when dryout of the affected steam generator is calculated to occur for this Design Basis MSLB event. This run time of 100000 seconds is well past the end of significant mass and energy release into the containment. Generally a run time of 1000 seconds is adequate to show that the containment pressure and temperature are decreasing rapidly and well below the peak values calculated prior to steam generator dryout. For this calculation, however, the run time has been extended to 100,000 seconds to provide insight into the long-term post-MSLB containment depressurization and cooldown to near pre-MSLB conditions.

b. ITEM 3: INITIAL CONTAINMENT PRESSURE

SONGS Units 2 and 3 Technical Specifications limit the containment pressure to between +1.5 psig and -0.3 psig during reactor operations (LCO. 3.6.1.4. references 6.6 and 6.7). Leakage of instrument air from valves and controllers cause containment pressure to normally be greater than 0 psig. Of the calculated post-MSLB containment conditions for equipment qualification, the peak vapor temperature is more limiting than the peak pressure. This is due to the fact that the calculated peak pressure is less than the design value of 60 psig and the short-term peak vapor temperature typically exceeds the containment design value of 300 °F. Based on sensitivity studies reported in the Bechtel Topical Report BN-TOP-3 (reference 6.8), the peak vapor temperature increases with decreasing initial containment pressure. Since the containment pressure is not normally less than atmospheric, an initial containment pressure of 14.7 psia (0 psig) will be used for this analysis.

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CCN CONVERSION

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

CCN NO. CCN -

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	
A	ALLEN EVINAY	11/04/94	PAUL BARBOUR	11/04/94						١,
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4.3 CARD SERIES 5

The last two entries on this card (0 and 105) are deleted. The G1-15 (RISC) version of COPATTA does not utilize these entry locations

4.3.a ITEM 3: CONTAINMENT EMERGENCY AIR COOLER START TIME

In the present analysis, the air cooler start delay time has been increased from 15 seconds to 50 seconds to coincide with the containment spray actuation time. The increase in air cooler start delay time will provide margin to accommodate potential changes in the timing of ECU startup such as an increase in the stroke time of the CCW block valves that isolate the cooling water from the air coolers.

4.4 CARD SERIES 301

No changes are made to card series 301 input which provides the mass flow rate and fluid enthalpy entering the containment from the main steam line break. The data is for the Design basis MSLB at 102% power with a break area of $7.48~{\rm ft}^2$.

As documented by CCN 1 to N-4080-004 (reference 6.3) and CCN 1 to N-4080-007 (reference 6.13), single failure of one of the isolation valves (HV8200 and/or HV8201) on the steam line feeding the auxiliary feed water pump turbine could allow cross-flow of steam from the intact steam generator into the containment through the affected steam generator. This cross-flow would come from the 1" diameter bypass lines installed around steam line check valves 1301MU003 and 1301MU005 by the MMP 2 & 3 6869.00SM. This potential additional mass and energy input is not included in this new AOR. The referenced CCNs demonstrate that the effect of the cross-flow on short-term peak containment conditions is not significant. The increase in peak pressure and peak temperature due to this potential cross-flow are less than 0.1 psi and 0.3 °F, respectively.

Similarly, a single failure of the containment isolation valve on instrument air or high/low nitrogen supply lines to close, coupled with a MSLB-induced failure of one of the supply or distribution lines inside the containment would also lead to additional mass and energy release beyond what is provided by ABB-CE. CCN 2 to N-4080-007 (reference 6.13) evaluated this single failure and concluded that there would be no significant impact to the short-term peak containment pressure or temperature. Therefore, the mass and energy releases from a failed air or nitrogen line is not included in this new equipment qualification AOR.

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CON CONVERSION

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

Subject CONTAINMENT P/T DESIGN BASIS MSLB FOR EQUIPMENT QUALIFICATION Sheet No. A-20

REV	CRIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	
A	ALLEN EVINAY	11/04/94	PAUL BARBOUR	11/04/94						
										'

4.5 CARD SERIES 801

No changes are made to card series 801 input except:

a.2(a) Containment Spray Injection Mode Spray Flow Rate

The minimum Containment Pump Spray Flow Rate has been changed to 1606 gpm (reference 6.2). In this calculation we use a value of 1600 gpm for further conservatism. Using the same criteria as in the AOR, this value translates to a flow rate of $7.956E+5\ lb/hr$.

The containment spray flow is discontinued at 1E4 seconds, consistent with a calculated time to deplete the refueling water storage tank inventory, using a single spray train, of about 1.1E4 seconds (reference 6.1, section 4.5.b.1). Following spray termination, containment heat removal is provided by the continued operation of the single train emergency air cooler units (2ECUs).

4.6 CARD SERIES 1101

The G1-15 (RISC) version of COPATTA does not have the option of multiple tables of ECU performance versus containment temperature for various values of cooling water supply temperature. Therefore, following the card series identifier (\$LIST POOL=1101), the input consists data pairs of containment saturation temperature and ECU heat removal rate.

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CCN CONVERSION CCN NO. CCN -

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

Subject CONTAINMENT P/T DESIGN BASIS MSLB FOR EQUIPMENT QUALIFICATION Sheet No. A-21

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	Г
A	ALLEN EVINAY	11/04/94	PAUL BARBOUR	11/04/94						
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A) Marine San Control									1	1

5.0 METHODOLOGY

The MSLB for Equipment Qualification evaluated in this calculation is the design basis $7.48~{\rm ft}^2$ steam line break accident at 102% power with off-site power available and with a loss of one train each of containment emergency air coolers and containment sprays.

The evaluation used the Bechtel COPATTA computer code (reference 6.5) to simulate the containment response to the MSLB.

The methodology employed in this calculation is identical to the present AOR (reference 6.1) for the Containment P/T Design Basis MSLB, with the exception that 8 percent condensate revaporization is added to the model to comply with NUREG-0588 design criteria to generate results applicable to equipment qualification evaluations.

In addition, the analysis run time is extended to 100,000 seconds (~28 hours) to provide insight into the long-term depressurization and cooldown of containment following the dryout of the affected steam generator and termination of containment spray flow at about 3 hours post-MSLB, when the refueling water storage tank has been exhausted. After spray termination, containment heat removal is provided by the continued operation of the single train emergency air cooler units (2ECUs). The long-term analysis is conservative since evaporative and convective heat transfer between the containment sump water and the vapor region is not modelled in this analysis.

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CCN CONVERSION

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

Subject CONTAINMENT BY DESIGN DAGIS MS B FOR POUTPMENT ONLY WIT

CCN NO. CCN -

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	
A	ALLEN EVINAY	11/04/94	PAUL BARBOUR	11/04/94						
								-		

6.0 REFERENCES

- 6.1 SONGS Units 2&3 Calculation N-4080-027, Revision 0, "Containment P/T Analysis for Design Basis MSLB", January 13, 1994.
- 6.2 SONGS Units 2&3 Calculation M-0014-009, Revision 0, Supplement A, "Containment Spray (CSS) In Service Minimum Requirements, July 28, 1994.
- 6.3 1) NCR 93030001-03
 - 2) NCR 93030002-02
 - 3) NCR 93030003-02
 - 4) NCR 93030004-02
- 6.4 SONGS Units 2&3 Calculation N-4080-004, Revision 1, "Equipment Qualification Thermal Analysis (MSLB), January 6, 1978 (includes CCN 1).
- 6.5 Bechtel Standard Computer Program, NE100, COPATIA, Version G1-15, "Containment Temperature and Pressure Transient Analysis", User and Theory Manuals.
- 6.6 SONGS Unit 2 Operating License and Technical specifications, up to and including Amendment 101.
- 6.7 SONGS Unit 3 Operating License and Technical specifications, up to and including Amendment 90.
- 6.8 Bechtel Topical report BN-TOP-3, Revision 4, "Performance and Sizing of Dry; Pressure Containments", March 1983.
- 6.3 NUREG-0588, Revision 1, "Interim Staff Position On Environmental Qualification of Safety-Related Electrical Equipment", July 1981.
- 6.10 SONGS Units 2 and 3 Calculation M-DSC-243, Revision 0, "Thermal Lag Analysis of Electrical Equipment at SONGS 2 & 3 due to MSLB", December 23, 1991.
- 6.11 SONGS Units 2 and 3 CCN 1 to Calculation M-DSC-243, Revision 0, "Thermal Lag Analysis of Electrical Equipment at SONGS 2 & 3 due to MSLB", January 15, 1992.
- 6.12 SONGS Units 2 and 3 Calculation M-0072-036, Revision 0, "Containment Emergency Cooler Performance Verification", December 9, 1993.

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CCN CONVERSION

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

CCN NO. CCN - 1

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	Г
1	ALLEN EVINAY	11/04/94	PAUL BARBOUR	11/04/94						١,
			***		-					١,

- 6.13 SONGS Units 2 and 3 Calculation N-4080-007, Revision 2, "Containment Pressure and Temperature from MSLB at various Power Levels", April 21, 1983 (includes CCNs 1 and 2).
- 6.14 Memo from J.1. Rainsberry to A.J. Brough, "Peak Containment Pressure Calculations, San Onofre Nuclear Generating Station, Units 2 and 3", May 12, 1994.
- 6.15 SONGS Units 2 and 3 Calculation N-4080-003, Revision 5, "Containment Spray (CSS) and Emergency Cooling Unit (ECU) Actuation Times", December 23, 1993
- 6.16 SONGS Units 2&3 Calculation N-40806027, Revision 0, "Containment P/T Analysis for Design Basis LOCA", January 28, 1994.

NES&L DEPARTMENT CALCULATION SHEET

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CCN CONVERSION

Project or DCP/MMP SO! GS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

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EV	CONTAINME!	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	-
1	ALLEN EVINAY	11/04/94	PAUL BARBOUR	11/04/94			-	1116	DAIL	
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7.	NOMENCLAT	URE								
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ICCN NO./ PRELIM. CCN NO.

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CCN CONVERSION CCN NO. CCN -

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

Subject CONTAINMENT P/T DESIGN BASIS MSLB FOR EQUIPMENT QUALIFICATION Sheet No. A-25

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	
A	ALLEN EVINAY	11/04/94	PAUL BARBOUR	11/04/94						

8.0 CALCULATION

8.1 COPATTA CODE INPUT DATA

COPATTA input data for the Containment P/T Design Basis MSLB Analysis for Equipment Qualification uses the Containment P/T Design Basis MSLB Analysis (reference 6.1) input data with modifications to reflect changes in containment spray flow rate (reference 6.2), initial containment pressure and condensate revaporization fraction to generate containment temperature and pressure profiles for the Equipment Qualification Thermal Analysis. Only the changes to the reference 6.1 input data will be presented in the following subsections.

8.1.1 TITLE CARD

*EQMSLB 102P, Pi=14.7, EV=8%, CT=1, TC=50, LOP=0, CS=1600, N-4080-027-SUP-A

8.1.2 CARD SERIES O

No changes made to Card Series 0 of reference 6.1 other than the deletion of the last four zero entries on the Bechtel input file as non-applicable to COPATTA version G1-15.

8.1.3 CARD SERIES 1: General Problem Information

&LIST POOL=1,1E5,14.7,2.305E6,120,0.6,20,582.945,1,1,0.08,14.7,0,0.50 \$END

ITEM 2:

TNFL = 2E4 seconds (per 4.2.a)

ITEM 3:

PAIR = 14.7 psia

The initial containment pressure before the MSLB mass and energy release is set to 14.7 psia for EQ calculations, as discussed in the Design Input Item 4.2.b.

Card Series input ITEMS 4 through 10 remain unchanged from that of reference 6.1.

ITEM 11: EVAP = 0.08

The fraction of heat sink condensate which will be allowed to revaporize is set to 0.08. Credit for revaporization will be taken for the purposes of EQ analysis per assumption 3.1.a.

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Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

CCN CONVERSION CCN NO. CCN -

Subject CONTAINMENT P/T DESIGN BASIS MSLB FOR EQUIPMENT QUALIFICATION Sheet No. REV ORIGINATOR DATE IRE DATE REV ORIGINATOR DATE IRE DATE ALLEN EVINAY 11/04/94 PAUL BARBOUR 11/04/94

8.1.4 CARD SERIES 5: Air Cooler Information

\$LIST POOL=5,2,50,1E7,0,0 \$END

ITEM 3: This item reflect the change of Containment Air Cooler start time from 15 seconds to 50 seconds as discussed in Design Input Item 4.3.a. No other changes have been made to this card data.

8.1.5 CARD SERIES 801: (Table 9)

This Card Series reflect the change of Containment Spray System (CSS) Flow Rate from $1612~\rm gpm$ to $1600~\rm gpm$ and the termination of containment spray flow at $10,000~\rm seconds$.

\$LIST POOL=801,

0, 0, 0, 0, 100, 100. 0, 50. 0, 0, 100, 100, 0, 0, 50, 7.956E5, 100. 100. 0, 0, 1E4, 7.956E5, 100. 100. 0, 0, 1E4. 0.0. 100, 100, 2E7, 0.0. 0. 0. 100, 100 \$END

8.1.6 CARD SERIES 1101

Items 2.3 and 4 of reference 6.1 input are deleted as not applicable to the G1-15 (RISC) version of COPATTA.

All other input used in this calculation remain unchanged from that of Reference 6.1, as described in Sections 8.1.1 through 8.1.33, except as changed in the preceding paragraphs.

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CON CONVERSION .

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

Subject CONTAINMENT P/T DESIGN BASIS MSLB FOR EQUIPMENT QUALIFICATION Sheet No. REV **ORIGINATOR** DATE IRE DATE REV ORIGINATOR DATE IRE DATE ALLEN EVINAY 11/04/94 PAUL BARBOUR 11/04/94

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2 0
9.0
      COPATTA INPUT FILE
*EQMSLB 102P, Pi=14.7, EV=8%, CT=1, TC=50, LOP=0, CS=1600, N-4080-027-SUP-A
 $LIST POOL=0,0,1,0,1 $END
 $LIST POOL=1,1E5,14.7,2.305E6,120,0.6,20,582.945,1,1,0.08,14.7,0.5 $END
 $LIST POOL=2,0,0,0,0,120,2E7 $END
 $LIST POOL=3,0,0,0,0,0,2E7,0,0,0,0 $END
 $LIST POOL=4,0,0,0,0,0,0,0,0,0,0,0,0 $END
 $LIST POOL=5,2,50,1E7,0,0 $END
 $LIST POOL=6,0,0,0 $END
 $LEAK NOPEN=0 $END
 $LIST POOL=101,
          0,
                  O SEND
        2E7,
 $LIST POOL=201,
                  0,
          0,
        2E7,
                  O SEND
 $LIST POOL=301,
                    0,
                           5.145520E7.
                                          1.195589E3.
                 0.22,
                           4.869032E7,
                                          1.197482E3.
                          4.622234E7,
                 0.42,
                                          1.198466E3.
                 0.62,
                          4.405936E7,
                                          1.199410E3.
                 1.08,
                          4.003276E7,
                                          1.201595E3.
                          3.688855E7,
                 1.58.
                                          1.201757E3,
                 2.08.
                          3.445970E7,
                                          1.202018E3.
                 2.58.
                          3.326288E7,
                                          1.200986E3,
                 3.58.
                          3.152606E7.
                                          1.201058E3.
                           3.028468E7,
                 4.58.
                                          1.201655E3,
                 5.58,
                          2.940080E7,
                                          1.201123E3.
                 6.58,
                          2.874870E7.
                                          1.201126E3,
                 7.58.
                          2.706574E7.
                                          1.204404E3.
                          2.468326E7,
                 8.58.
                                          1.204367E3,
                 9.58.
                          2.294968E7,
                                          1.204238E3,
                          2.160122E7,
                10.58.
                                          1.203908E3,
                12.58.
                          1.943143E7,
                                          1.203195E3,
                14.58.
                           1.765940E7,
                                          1.202277E3.
                16.58,
                          1.637240E7.
                                          1.201556E3.
                          1.544720E7,
                18.58.
                                          1.200963E3.
                20.58.
                           1.473293E7.
                                          1.200422E3.
                25.58.
                          1.327525E7.
                                          1.198820E3.
                30.58,
                          1.221858E7,
                                          1.197825E3.
                35.58.
                           1.146406E7,
                                          1.196753E3.
                40.58.
                          1.059131E7.
                                          1.195307E3.
                45.58,
                          9.801216E6,
                                          1.194165E3.
                50.58,
                          9.132588E6.
                                          1.193086E3,
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CCN CONVERSION CCN NO. CCN -

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

CCN NO. CCN - X

EV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	
2	ALLEN EVINAY	11/04/94	PAUL BARBOUR	11/04/94					1	1
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		60.58.	8.28032	4F6.	1.190	935F3				1
		61.08,	7.245576	5E6.	1.190	949E3.				1
		62.08,	5.803344	4E6,	1.189	165E3,				1
		62.58,	3.23870	4E6,	1.184	658E3,				
		64.58,	7.245576 5.803344 3.238704 3.948846	0E5,	1.179	953E3,				
		68.58,	1.074240	DE5,	1.251	072E3,				1
		/1.08,		0,		0,				
\$1	IST POOL=401	2E7,		0,		0 \$END				
4	0,	0,	0,							
	2E7,	0,	O SEND							
\$L	IST POOL=501	,								
	0,	0,	0,							
٠.	2E7,		0 \$END							
\$L	IST POOL=601	, , ,,,,,								
	0,	7.2E4	7.2E6	,						
	0.05,	7.2E4	, 7.250),						
	0.05, 2E7,	0.0	0 \$END	,						
\$L	IST POOL=701	. ,	O PLIND							
	0,	0,	0, 0,							
	2E7.	0.	0, 0	\$END						
\$L	IST POOL=801									
	0,				100,					
	50,				100,					
	50, 7.95 1E4, 7.95	6E5,			100, 100,					
	1E4,	0.0.			100,					
	2E7,	0.0,			100 \$E!	ND				
\$1.	IST POOL=901	,								
		0,	0,							
41	2E7, IST POOL=100		0 \$END							
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			2.0 \$END							
\$L	IST POOL=110	1,								
		,	0,							
		, 1.670								
		, 3.020								
		, 4.570								
		, 8.27								
		, 1.040								
		, 1.27								
		, 1.523								
		, 1.788								

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Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

CCN CONVERSION CCN NO. CCN - 1

EV	ORIGINATOR	DATE	IRE	DATE	REV	JIPMENT QUAL ORIGINATOR	Section 14 (Section 2019) The Control of the Contro	CHARLES CHARLES AND A STREET	INCOMMENDATION AND PERSONS IN	A- 29
8	ALLEN EVINAY	11/04/94	PAUL BARBOUR	11/04/94	HE.V	ORIGINATOR	DATE	IRE	DATE	1 .
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	210	, 2.06	8E7.							
	220	, 2.36	1E7,							
	230	, 2.66	4E7,							
	240	, 2.97	4E7,							
	250	, 3.29	1E7,							
	250	, 3.61	IE/,							
	280	, 3.93	1E/,							
	287	, 4.47	4F7.							
		, 4.56								
	300	, 4.88	2E7 \$END							
\$L	IST P00L=120									
		, 0.72								
		, 0.73								
		, 0.74								
	0.4	, 0.77	1							
		, 0.78								
	0.6	, 0.809	9,							
		, 0.83								
		, 0.86								
		, 0.912								
		, 0.983								
		0.99								
	1.3	, 1.000								
\$L	IST POOL=900									
		5, 0.0	05, 1.0,	400						
		10, 0.0	05, 1.0,							
		20. 0.0	05, 1.0, 05, 1.0,	5,						
	1	00, 0	1, 1.0,	5,						
	21	00, 1.	.0, 5.0,	5.						
	61	00, 1	.0, 10.0,	5,						
	80	00, 2	.0, 20.0,							
	11	13, 5,	.0, 50.0, .0, 1000,							
	11	F4. 50.	0, 500,	2,						1
	51	E4, 50.	0, 5000,	2,						
	21	E5, 50.	0, 10000,	2 \$E	ND					
	IST POOL=9999	9 \$END								
* H:	S #1 - REACT(OR BUILD	ING DOME							
\$L	IST POOL=1010	101, 100	0, 0, 0, 0,	0, 0,	34693	.22 \$END				
4 L	IST POOL=101	3	0.00075,	10 0	06360	3,				
		20.	0.23028,	37. 1	.00300)				
			, , ,			,				1

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CCN CONVERSION

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

CCN NO. CCN - 1

EV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	
A	ALLEN EVINAY	11/04/94	PAUL BARBOUR	11/04/94						1 10
										É
\$L \$L * H \$L \$L	IST POOL=101 IST POOL=101 IST POOL=101 IST POOL=102 IST POOL=102 IST POOL=102 IST POOL=102 IST POOL=102	201, 4, 300, 0, 400, 9, DER WAL 001, 10 101, 5, 20, 21, 201, 4,	0 \$END 2, 1, 1 \$1 L BETWEEN 1 0, 7, 0, 0 0.00075, 0.02193, 0.14694, 4.35526 \$1 1, 5, 2, 2	END E1. 29'6 , 0, 0, 3, 0 10, 0 37, 0.	38120 38120 0.0215 0.0636 91776	\$END 8, 0,				
\$L * H \$L	IST POOL=102 IST POOL=102 S #3 - CYLIN IST POOL=103 IST POOL=103	400, 9, DER WAL 001, 10 101, 5, 3, 20,	2, 1, 1 \$1 L BETWEEN B 0, 7, 0, 0, 0.00075, 0.02193, 0.14694,	E1. 15'(, 0, 0, 3, (10, (37, 0.	6667. 0.0215 0.0636	38 \$END 8, 0,				
\$L \$L * H \$L	IST POOL=103 IST POOL=103 IST POOL=103 S #4 - BASEM IST POOL=104 IST POOL=104	201, 4, 300, 0, 400, 9, AT (OTH 001, 53 101, 3, 20,	0 \$END 2, 0, 2 \$ER THAN REA 5, 0, 0, 0.00067, 1.52698,	2, 2, 2 END ACTOR BA 0, 0, 1	SEMAT 12800 0.1	\$END				
\$L \$L * H \$L	IST POOL=104 IST POOL=104 IST POOL=104 S #5 - REACT IST POOL=105 IST POOL=105	201, 4, 300, 0, 400, 3, OR BASE 001, 70 101, 4,	0 \$END 3, 0, 3 \$E MAT & S.G. , 4, 0, 0,	END PEDESTA 0, 0, 1	0.1					
\$L * H \$L	IST POOL=105 IST POOL=105 IST POOL=105 S #6 - REACT IST POOL=106 IST POOL=106	201, 4, 300, 0, 400, 3, OR CAVI 001, 93 101, 5, 30,	2, 2, 2 \$1 0 \$END 3, 0, 3 \$1 TY WALLS B1 , 5, 1, 11	END ELOW E1. .75, 0, 7, 1	15'0 0, 21	" .5 \$END 92.				
\$L \$L	IST POOL=106 IST POOL=106 IST POOL=106 S #7 - REACT	201, 4, 300, 0, 400, 3,	2, 2, 2, 2 0 \$END 3, 0, 3 \$1	2 \$END END						

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CCN CONVERSION

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

CON NO. CON -

EV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	T-
1	ALLEN EVINAY	11/04/94	PAUL BARBOUR	11/04/94			: 272			BDCATE
										•
							-	-		
\$1	LIST POOL=107	001, 68	, 5, 0, 0,	0, 0, 2	2810 \$	END				
\$1	LIST POOL=107	101, 5,	0.00192,	7, 0.0	02292,					
		20.	0.40192, 4.00192 \$1	END.	2.00,					
\$1	LIST POOL=107	201, 4,	2, 2, 2, 1	2 \$END						l
\$1	IST POOL=107	300, 0,	0 \$END	TND						
* +	IST POOL=107 HS #8 - LINED	REFUEL	ING CANAL N	WALLS						
\$1	IST POOL=108	3001. 86	. 6. 0. 0.	0. 0. 9	9200 \$	END				
\$1	LIST POOL=108	101, 5,	0.01563,	20,	0.	1,				
		20	0.41563,	20,	2.0	O,				
201	131 PUUL=108	5201. 3.	1. 7. 7. 1	2. 4 SEI	4.01/5 VD	2 PEND				
31	LIST POOL=108	300. 0.	O SEND							
* \$1	IST POOL=108	3400, 9,	2, 9, 2 \$1	END	DEEL C	NI HALLS OTH	TAIT			
\$1	HS #9 - S.G. LIST POOL=109	001. 78	4. 0. 0.	0. 0. 4	11976	SEND	INI WALL	-5		
\$1	IST POOL=109	101, 5,	0.00192,	10, 0	0.0423	3,				
		12,	0.1,	50.	.7187	6 \$END				
SI	IST POOL=109 IST POOL=109	300. 0	0 \$FND	END						
\$1	LIST POOL=109	400, 9,	2, 0, 2 \$1	END						
* +	HS #10 - FL00	R SLABS	(OTHER TH	AN BASEN	MATS)					
\$1	LIST POOL=110 LIST POOL=110	0001, 67	, 6, 0, 0,	0, 0, 1	17474	\$END				
ΨL	_131 FOOL-110	20.	0.105348,	15. 0.5	505348					
	122 222	20,	1.505348,	3, 1.50	06015	\$END				
\$1	IST POOL=110 IST POOL=110	201, 4,	1, 2, 2, 2	2, 4 \$E	ND					
\$1	IST POOL=110	400. 9.	2. 9. 2 \$1	FND						
* +	4S #11 - LIFT	ING DEV	ICES (EXCE	PT STAIN						
\$1	_IST_POOL=111	001, 17	, 2, 0, 0,	0, 0, 5	57286	\$END				
\$1	_IST POOL=111 _IST POOL=111	201 4	1 \$FND	10, 0.04	17:317	\$END				
	IST POOL=111									
	LIST POOL=111									
	HS #12 - MISC LIST POOL=112						INCHES			
\$1	IST POOL=112	101, 6.	0.0005, 1	7. 0.084). 1.	ND				
		15,	0.20, 25,	0.31084		D				
	IST POOL=112			END						
	_IST POOL=112 _IST POOL=112			END						
* +	HS #13 - MISC	ELLANEO	US CARBON S	STEEL: 1			50"			
\$1	_IST_POOL=113	001, 32	, 2, 0, 0,	0, 0,	12042	\$END				
D	_IST POOL=113	1111 h	11 (1()())	en 11 16						

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CON CONVERSION

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

CCN CONVERSION

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	T
2	ALLEN EVINAY	11/04/94	PAUL BARBOUR	11/04/94						
		L								'
\$1	IST POOL=113 IST POOL=113	201, 4,	1 \$END							
\$1	IST POOL=113	400, 9,	2, 0, 2 \$1	END						
\$1	HS #14 - MISC LIST POOL=114	001, 19	, 2, 0, 0,	0, 0, 6).50"< 64693	THICKNESS<1.	00"			
\$1	IST POOL=114 IST POOL=114	101, 5,	0.000674,	13, 0.0	38607	\$END				
\$1	LIST POOL=114	300, 0,	0 \$END							
* 1	IST POOL=114 IS #15 - MISC	400, 9,	2, 0, 2 \$1	END STEEL - T	HICKN	FSS<0 5"				
\$1	IST POOL=115	001, 17	, 2, 0, 0,	0, 0, 9	8913.	6 \$END				
\$1	IST POOL=115 IST POOL=115	101, 6,	0.000606, 1 \$FND	10, 0.0	12833	\$END				
\$1	.IST POOL=115	300, 0,	O \$END							
* +	IST POOL=115 IS #16 - ELEC	TRICAL	2, 0, 2 \$FOUTPMENT	END						
\$1	.IST POOL=116	001, 8,	1, 0, 0, (0, 0, 37	644.5	\$END				
	IST POOL=116 IST POOL=116			ND						
\$1	IST POOL=116	300, 0,	0 SEND							
* 1	IST POOL=116 IS #17 - MISC	400, 9,	2, 0, 2 \$8	ND S STEEL						
\$1	IST POOL=117	001, 16	. 1. 0. 0.	0. 0. 2		\$END				
\$L \$L	IST POOL=117 IST POOL=117	101, 15, 201, 3	, 0.01747 \$	END						
\$1	IST POOL=117	300, 0,	O SEND							
* +	IST POOL=117 IS #18 - UNLI	400, 9, NED REFI	2, 0, 2 \$8	END LI WALLS	RELO	W F1 63'6"				
\$L	IST POOL=118	001, 48.	. 4. 0. 0.	0. 0. 3	700 \$	END				
\$L	IST POOL=118	101, 5,	0.00192, 7	0.022	92,	END				
\$L	IST POOL=118	201, 4,	2, 2, 2 \$8	ND	172 4	LIND				
\$L \$L	IST POOL=118 IST POOL=118	300, 0, 400. 9.	0 \$END	ND						
* +	S #19 - REAC	TOR BLDO	G CYLINDER	#3: SEC	TIONS	WITH STIFFE	NERS			
\$1	IST POOL=119 IST POOL=119	001, 100 101, 5	0, 7, 0, 0,	0, 0,	1590.	68 \$END	56777			
	10.1000	15,	0.70944,	20, 0	.7927	8, 16, 1.44	4278,			
\$1	IST POOL=119		4.87885 \$E		\$FND					
\$L	IST POOL=119.	300, 0,	0 \$END		4 CIAD					
\$L	IST POOL=119 S #20 - VENT	400, 9, TUNNELS	2, 1, 1 \$E	ND						
* H	77 Mar 17 Table 1 1									
* H	IST POOL=120 IST POOL=120	001, 23,	, 2, 0, 0,	0, 0, 2	827 \$1	END				

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CCN CONVERSION 1

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

\$LIST POOL=120300, 0, 0 \$END \$LIST POOL=120400, 9, 2, 0, 2 \$END \$LIST POOL=410001, 25, 54, 0.8, 30, 10, 54, 0.1, 20, 0.0174, 0.0103 \$END \$LIST POOL=500000 \$END

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Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

CON CONVERSION CON NO. CON - 1

Subject CONTAINMENT P/T DESIGN BASIS MSLB FOR EQUIPMENT QUALIFICATION Sheet No. A-34

REV ORIGINATOR DATE IRE DATE REV ORIGINATOR DATE IRE DATE

ALLEN EVINAY 11/04/94 PAUL BARBOUR 11/04/94

ALLEN EVINAY 11/04/94 PAUL BARBOUR 11/04/94

10.0 SELECTED OUTPUT DATA

The tabulated data presented in Sections 10.1 and 10.2 consists of partial output of the COPATTA calculation made for this analysis.

10.1

	CONTAINMENT	CONTAINMENT	CONTAINMENT	HEAT SINK
TIME	PRESSURE	VAPOR TEMP	SUMP TEMP	(LEFT BOUND)
(SEC)	(PSIG)	(F)	(F)	(F)
0	0.00	120.00	120.00	118.4
1	3.59	179.50	136.10	118.4
2	6.50	218.40	151.70	
3	9.05	246.80	162.70	
4	11.42	269.40	171.40	
5	13.67	288.00	178.80	136.0
6	15.81	303.70	185.20	
7	17.86	317.20	190.80	
8	19.79	328.70	195.90	
9	21.54	338.30	200.30	
10	23.13	346.20	204.20	153.4
11	24.59	352.90	207.70	
12	25.96	358.70	211.00	
13	27.24	363.70	213.80	
14	28.43	368.00	216.40	
15	29.55	371.80	218.70	166.6
16	30.61	375.10	220.90	

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CCN CONVERSION CCN NO. CCN -

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	
A	ALLEN EVINAY	11/04/94	PAUL BARBOUR	11/04/94						W

	CONTAINMENT	CONTAINMENT	CONTAINMENT	HEAT SINK
TIME	PRESSURE	VAPOR TEMP	SUMP TEMP	(LEFT BOUND)
(SEC)	(PSIG)	(F)	(F)	(F)
17	31.61	378.10	223.00	
18	32.56	380.70	224.90	
19	33.47	383.00	226.60	
20	34.37	385.14	228.30	178.4
22	36.05	388.86	231.30	
24	37.60	391.95	233.90	
25	38.34	393.10	235.20	
26	39.06	394.37	236.30	
28	40.46	396.56	238.50	
30	41.80	398.44	240.50	195.9
32	43.07	400.06	242.30	
33	43.69	400.80	243.20	
34	44.29	401.47	244.00	
36	45.47	402.70	245.60	
38	46.60	403.76	247.00	
40	47.68	404.64	248.40	209.9
42	48.71	405.36	249.70	
44	49.69	405.95	250.90	
45	50.16	406.20	251.50	
46	50.63	406.42	252.10	
48	51.52	406.78	253.20	
50	52.38	407.07	254.20	222.2
52	52.93	402.84	255.20	

NES&L DEPARTMENT CALCULATION SHEET

ICCN NO./

PRELIM. CON NO. N-1

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CCN CONVERSION CCN NO. CCN -

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

Subject CONTAINMENT P/T DESIGN BASIS MSLB FOR EQUIPMENT QUALIFICATION Sheet No. 4-36

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	
A	ALLEN EVINAY	11/04/94	PAUL BARBOUR	11/04/94						
					CONTRACT LINES	THE PERSON NAMED IN COLUMN TWO IS NOT THE OWNER.		***************************************	1	

	CONTAINMENT	CONTAINMENT	CONTAINMENT	HEAT SINK
TIME	PRESSURE	VAPOR TEMP	SUMP TEMP	(LEFT BOUND)
(SEC)	(PSIG)	(F)	(F)	(F)
54	53.46	398.66	256.20	
56	53.97	394.58	257.10	
58	54.46	390.62	258.00	
60	54.93	386.75	258.80	231.8
62	55.27	382.72	259.50	
64	54.97	377.40	260.30	
66	54.35	371.49	260.90	
68	53.71	365.60	261.40	
70	53.06	359.64	261.90	236.2
75	51.47	345.04	262.90	
80	50.02	331.06	263.60	238.2
85	48.58	317.22	264.10	
90	47.21	303.72	264.40	239.6
95	45.89	290.55	264.70	
100	44.62	277.64	264.90	240.4
105	43.70	269.19	265.00	
110	43.22	268.35	265.20	
115	42.80	267.75	265.30	
120	42.40	267.16	265.40	
125	42.01	266.59	265.40	242.5
130	41.64	266.00	265.40	
135	41.28	265.51	265.40	
140	40.94	264.99	265.40	

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CCN CONVERSION CCN NO. CCN - 1

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

Subject CONTAINMENT P/T DESIGN BASIS MSLB FOR EQUIPMENT QUALIFICATION Sheet No. A-37 REV ORIGINATOR DATE IRE DATE REV ORIGINATOR DATE IRE DATE ALLEN EVINAY 11/04/94 PAUL BARBOUR 11/04/94 Nº

	CONTAINMENT	CONTAINMENT	CONTAINMENT	HEAT SINK
TIME	PRESSURE	VAPOR TEMP	SUMP TEMP	(LEFT BOUND)
(SEC)	(PSIG)	(F)	(F)	(F)
145	40.58	264.49	265.30	
150	40.28	264.00	265.20	243.5
155	39.97	263.52	265.20	
160	39.77	263.22	265.10	
165	39.48	262.76	265.00	
170	39.19	262.32	264.90	
175	38.91	261.88	264.80	243.8
180	38.59	261.40	264.70	
185	38.37	261.03	264.60	
190	38.11	260.62	264.50	
195	37.86	260.22	264.40	
200	37.61	259.82	264.30	243.6
250	35.44	256.25	263.10	242.4
300	33.76	253.34	261.80	241.1
350	32.23	250.61	260.50	239.6
400	30.90	248.15	259.20	238.1
450	29.70	245.86	258.00	236.5
500	28.69	243.87	256.70	235.0
550	27.68	241.81	255.40	233.5
600	26.72	239.82	254.10	232.0
700	24.99	236.06	251.40	228.8
800	23.52	232.69	248.80	225.9
900	22.12	229.33	246.10	223.1

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ICON NO./ PRELIM. CON NO. N-1

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CCN CONVERSION CCN NO. CCN -

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE
A	ALLEN EVINAY	11/04/94	PAUL BARBOUR	11/04/94					

	CONTAINMENT	CONTAINMENT	CONTAINMENT	HEAT SINK
TIME	PRESSURE	VAPOR TEMP	SUMP TEMP	(LEFT BOUND)
(SEC)	(PSIG)	(F)	(F)	(F)
1000	20.85	226.13	243.50	220.3
2000	13.76	204.75	224.10	
4000	6.19	169.41	199.70	172.3
8000	1.83	132.34	170.70	
9000	1.499	128.58	165.90	
10000	1.25	125.84	161.70	141.9
15000	1.17	144.67	161.50	
20000	0.97	143.49	161.39	140.0
40000	0.79	138.57	160.94	135.9
60000	0.72	135.46	160.52	
90000	0.57	132.61	159.94	130.4
1E+5	0.63	131.95	159.75	

ICCN NO./ PRELIM. CCN NO.

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CCN CONVERSION CCN NO. CCN - 1

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-w80-027-Sup-A

Subject CONTAINMENT P/T DESIGN BASIS MSLB FOR EQUIPMENT QUALIFICATION Sheet No. A-39

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	
A	ALLEN EVINAY	11/04/94	PAUL BARBOUR	11/04/94						. N
										**
			WATER SECTION							

10.2

TIME	INTEGRATED ENERGY REMOVED BY CONTAINMENT SPRAYS (a)	INTEGRATED ENERGY REMOVED BY CONTAINMENT AIR COOLERS (b)
secs	(btu)	(btu)
50	0.0e+00	2.30e+03
51	6.75e+04	2.53e+04
60	6.55e+05	2.36e+05
100	2.70e+06	1.15e+06
200	6.33e+06	3.23e+06
500	1.62e+07	8.77e+06
1000	2.96e+07	1.65e+07

- (a) Energy is transferred to containment sump water.
- (b) Energy is transferred to component cooling water (CCW) system.

TIME	ENERGY REMOVAL RATE BY CONTAINMENT SPRAYS	TIME	ENERGY REMOVAL RATE BY CONTAINMENT AIR COOLERS
secs	(btu/hr)xE6	secs	(btu/hr)xE6
51.5	241.5	50	82.7
60.0	227.8	60	85.4
99.5	142.2	100	78.6
200.0	127.0	200	72.1
500.0	110.3	500	61.8
975.0	086.0	1000	50.9

NES&L DEPARTMENT CALCULATION SHEET

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CCN CONVERSION

Project or DCP/MMP SONGS UNITS 2 and 3 Calc No. N-4080-027-Sup-A

CCN NO. CCN -

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	THE REAL PROPERTY.
A	ALLEN EVINAY	11/04/94	PAUL BARBOUR	11/04/94				-		*
								-	-	-

APPENDIX A (COPATTA Code I/O File)

The COPATTA Code input file is presented in Section 9 of this calculation.

The COPATTA Code output file is included on Microfiche. The output file name and date are as follows:

FICHE TITLE : EQMSLB J6908 02-Nov-94

JOB TITLE :

*MSLB 102%P, CPi=14.7, EVAP=8%, CT=1, LOP=0, CS=1600,

N-4080-027-SUP-A

RUN DATE :

11-02-94

LAST SHEET : Page 387

CA	LCULATIO	N TITLE P	AGE	PRELIM CCN NO.	PAGE OF
Calc. No. N-4080-0	27 DCP/M	MP/EIDCN/ECN	NI- O CO- NI/A	CCN CONVERSION	ON:
Subject CONTAINME				CCN NO. CCN	Sheet 1
System Number/Primar				SONGS Unit 2&3	- Contraction and
			1301		- Annual Control of the Control of t
Tech Spec Affecting?	NO X	YES, Section No.	. LCO 3.6.1.1/2/3 & B3.	6.1.4/6 Equipment Tag	No. N/A
CONTROLLED COMPUTER PROGRAM/ DATABASE	X PROGRA DATABA IN ACCORDANCE		PROGRAM/DATABASE X ALSO LIST 'COPATTA" MA	TED BELOW	ion G1/14
	THE THE SET OF THE SET		RECORD OF ISSUES		
REV.		TOTAL			
DESCR	LJCOUPIF HUJIV Innovenesses		APPROVED		
DISC		SHT.	(Print name/initial)		(Signature)
0 SEE NOTE 1 B		155 ORIG	ephen Oliver	(5) Balon	Other Der IPRE
BPC N ISSUED FOR U	JSE	155 IRE	ephen Oliver	- Fre AJ-Echh	DATE
	4	Jo	hn Elliott	A Song	_ 1-13-94
		ORIG		16#	Other
		IRE		t _{DM}	DATE
		ORIG		GS	Other
		IRE	AMERICAN SECURIO DE SECURIO SERVICIO AMERICAN ANCAS AN	рм	DATE
CONTRACTOR OF THE PROPERTY OF		ORIG		GS	Other
		IRE			DATE
			and a second supplementary and the second supplementary and analysis and the second supplementary and a supplementary and the second supplementary and supplementar		
Space for RPE stamp, iden Note 1: The purpose of Revision			tes as applicable.		
Revisions 0, 1 and 2 Open Item Reports Disclaimer: This c	Revision 0 to in an effort to im	this calculation (prove documenta repared using Wo	N-4080-027) will incorption and accuracy of the	icate discrepancies in Cal porate the recommended e MSLB P-T calculation. However, WP 5.1 was	changes specified by these
This calc. was prepared fo directing DCN conversion.				otance to be verified by reci no date	ept of a memorandum

CALCULATION CROSS INDEX

ICCN NO./
PRELIM. CCN NO.

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CCN CONVERSION:

Calculation No. N-4080-027

Sheet No. 2 CCN NO. CCN-

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1 PURPOSE

1.1 TASK DESCRIPTION

The purpose of this calculation is to evaluate the containment pressure and temperature response to a design basis Main-Steam-Line-Break (MSLB) for SONGS Units 2 and 3. The results of this calculation supersede the results of Calculation N-4080-007, "Containment Pressure Temperature from MSLB at Various Power Levels", (Reference 6.1.d) with respect only to the Design Basis MSLB event (7.4765 ft2 MSLB @ 102% power with failure of one cooling train). Per the conclusions presented in Calculation N-4080-007, this is the worst case MSLB, and will envelope all the other break types. The changes in design input and assumptions used in this calculation will not alter the relative severity of the different break scenarios, and thus the MSLB @ 102% power with failure of one cooling train will remain the limiting case.

Resolution of the following Open Item Reports require the results of this calculation:

OIR NO. PROPOSED RESOLUTION

- 92-015 Correct UFSAR Table 6.2-9 to accurately report the time of occurrence of the peak containment pressure. (Reference 6.9.a).
- 92-045 Revise the analysis of Calculation N-4080-007 to include the origin of input parameters or, if a source document can not be found, then justify the modeled value. Append copies of computer code input files to this calculation. (Reference 6.9.b).
- 92-054 Correct UFSAR Table 6.2-9 to accurately report containment pressures, temperatures and times of occurrence (Reference 6.9.c).
- 92-057 Revise the analysis of Calculation N-4040-007 to adequately document the peak containment temperatures (Reference 6.9.d).
- 92-059 Revise the analysis of Calculation N-4080-007 to correct a discrepancy in the RWST volume. Verify that the new results do not modify information presented in UFSAR section 6.2.1.1.3.1. (Reference 6.9.e)
- 92-069 Revise the analysis of Calculation N-4080-007 using the Uchida HTC instead of the Modified Tagami HTC (Reference 6.9f).

This calculation also addresses the reduced Containment Spray flowrates as described in disposition step 2 of NCRs 93030001, 93030002, 93030003, and 93030004. (References 6.16). This calculation incorporates the minimum spray flow identified in Calculation M-0014-009 (Reference 6.1.b).

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The Bechtel Standard Computer Code MAP-175, Release G1-14 (COPATTA) (Reference 6.5.a) will be used in this calculation to evaluate the pressure-temperature transients.

1.2 CRITERIA, CODES AND STANDARDS

The containment structure is to be designed such that it is capable of withstanding the adverse affects of a postulated MSLB. Applicable regulatory design criteria are provided in Appendix A to 10 CFR Part 50 (Reference 6.4.a). These criteria include:

- •General Design Criterion 16, "Containment Design"
- General Design Criterion 38, "Containment Heat Removal"
- General Design Criterion 50, "Containment Design Basis"

General Design Criterion 16 requires that a reactor containment and associated systems shall be provided to establish an essentially leak tight barrier to assure that the containment design conditions important to safety are not exceeded for as long as the conditions require. Per Standard Review Plan 6.2.1.1.A (Reference 6.4.c), to satisfy the requirements of this criterion, the calculated containment peak pressure after a MSLB should be less than the design containment peak pressure.

General Design Criterion 38 requires that the containment heat removal systems function to rapidly reduce the containment pressure following any LOCA, and maintain the pressure at an acceptably low level. Although not explicitly applied to the case of the MSLB, the requirements of GDC 38 can be considered to be applicable to the containment peak pressure analyses (be it LOCA or MSLB).

General Design Criterion 50 requires that the reactor containment structure, including access openings, penetrations, and the containment heat removal system, shall be designed so that the containment structure and its internal components can accommodate, without exceeding the design leakage rate and with sufficient margin, the calculated pressure condition resulting from a LOCA. As with Criterion 16, per Standard Review Plan 6.2.1.1.A, to satisfy the requirements of Criterion 50, the calculated containment peak pressure after a LOCA should be less than the design containment peak pressure. Although GDC 50 specifically addresses a LOCA, and not an MSLB, SRP 6.2.1.1.A indicates that the requirements of GDC 50 can be considered to be applicable to the containment peak pressure analyses (be it LOCA, steam or feedwater line break).

The containment design pressure is 60 psig and the containment design temperature is 300 °F per the Technical Specifications (References 6.3.a and 6.3.b, Section 5.2.2).

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2 RESULTS/CONCLUSIONS AND RECOMMENDATIONS

2.1 RESULTS/CONCLUSIONS

Figure 2-1 presents the sump and vapor pressures versus time for the DBA MSLB. The plots in Figure 2-1 are generated using the data presented in Section 10.1.

Figure 2-2 presents the containment gauge pressure versus time for the DBA MSLB. The plot in Figure 2-2 is generated using the data presented in Section 10.1.

Figure 2-3 presents the condensing heat transfer coefficient used by the COPATTA Code versus time for the DBA MSLB. The plot in Figure 2-3 is generated using the data presented in Section 10.1.

Figure 2-4 presents the inside surface temperature of heat sink 1 (reactor building dome) to represent the temperature of the containment structure. The plot in Figure 2-4 is generated using the data presented in Section 10.1.

Figure 2-5 presents the instantaneous energy vs. time data used by COPATTA to determine heat transfer in the DBA MSLB. The plots in Figure 2-5 are generated using the data presented in Section 10.2. Included are:

VAPOR ENERGY: Instantaneous steam+air energy.

SUMP ENERGY: Instantaneous energy of sump water.

TOTAL ENERGY: Instantaneous energy inventory.

HEAT SINKS:

Instantaneous energy stored in structures.

Figure 2-6 presents the integrated heat transfer of the air coolers and containment sprays. The plots presented in figure 2-6 are generated using the data in Section 10.2. Included are:

AIR COOLERS:

Integrated energy removed by emergency fan coolers.

CONT. SPRAY:

Integrated energy transferred to sump by sprays.

The following table presents the accident chronology for the analysis.

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TIME (seconds)	EVENT
0.0	Break occurs
15	Emergency fan coolers start (at full capacity)
50	Containment spray nozzles at full discharge flow
50.0	Peak containment temperature of 421 °F
62.3	Peak containment pressure of 58.5 psig
71.08	End of Blowdown

Note that although the peak vapor temperature of 421 °F is greater than the 300 °F design temperature, the duration of the event is sufficiently small to prevent heating of the containment structural materials beyond the design limits. As indicated by Figure 2-4, the 241 °F peak surface temperature of the containment liner remains well below 300 °F. Because the liner inside surface (actually a layer of organic paint) remains below 300 °F, the containment structure will not exceed design temperatures.

As can be seen from Figures 2-2 and 2-4, the peak pressure (58.5 psig) is below the design pressure of 60 psig and the peak temperature of the containment structure (241 °F) is below the design temperature of 300 °F. Therefore, General Design Criteria 16 and 50 (See Section 1.2) are met. The gauge pressure with respect to the outside atmosphere at 10,000 seconds is less than 3.0 psig. The pressure remaining after 24 hours is therefore expected to be only a small fraction of the 60 psig design pressure; therefore, the requirements of General Design Criterion 38 (See Section 1.2) are met.

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2.2 RECOMMENDATIONS

Since this calculation is the new analysis of record for the Design Basis MSLB Pressure Temperature analysis, it should be noted in calculation N-4080-007 (Reference 6.1.d) that the results of the 7.4765 ft2 MSLB at 102% power with one of two cooling trains available and offsite power available have been superseded by the results of this calculation.

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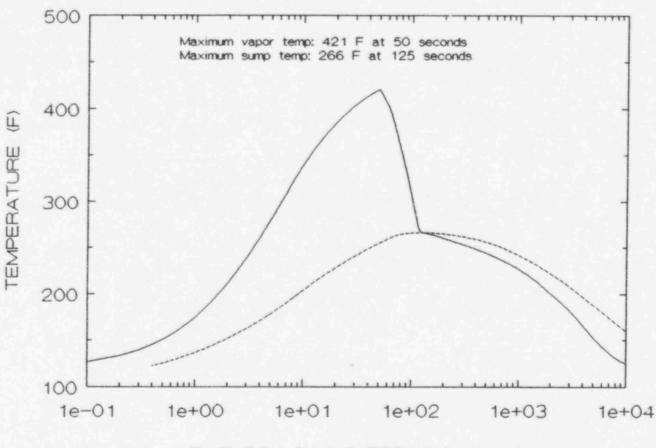
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FIGURE 2-1: TEMPERATURE MSLB 102% POWER, 7.48 FT2 BREAK AREA ----- SUMP VAPOR TEMP TEMP



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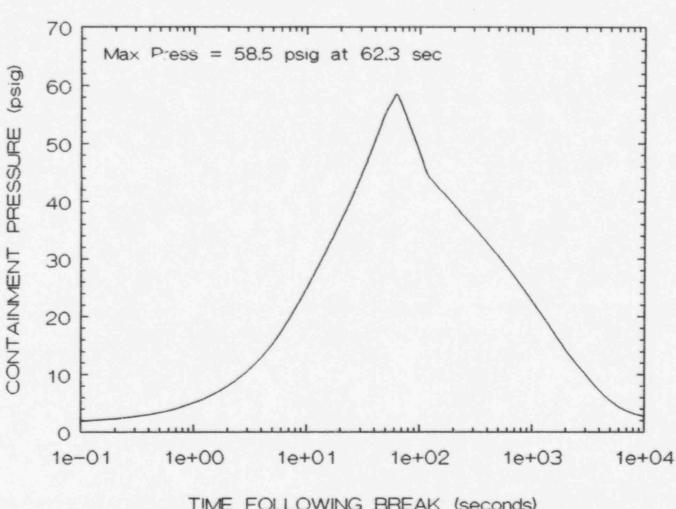
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FIGURE 2-2: CONTAINMENT PRESSURE MSLB 102% POWER, 7.48 FT2 BREAK AREA



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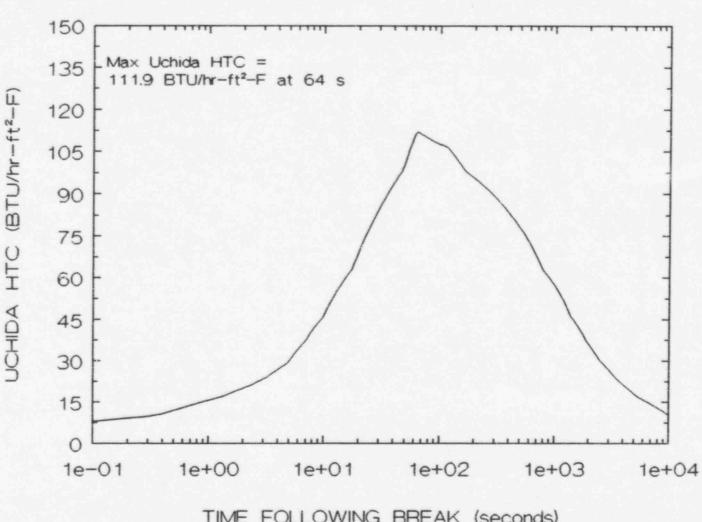
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FIGURE 2-3: CONDENSING HTC MSLB 102% POWER, 7.48 FT2 BREAK AREA



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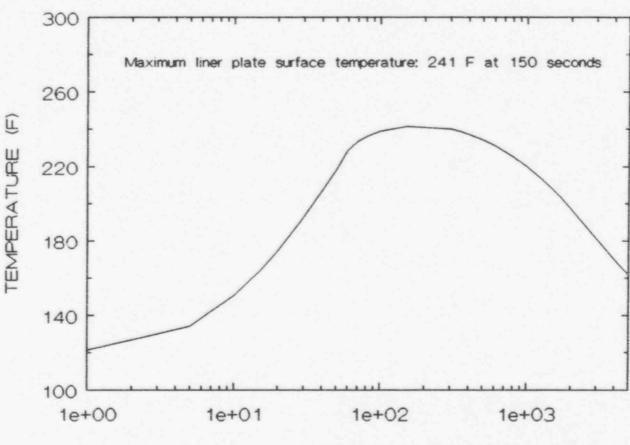
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FIGURE 2-4: LINER PLATE SURFACE TEMP. MSLB 102% POWER, 7.48 FT2 BREAK AREA HEAT SINK 1 (LEFT BOUND)



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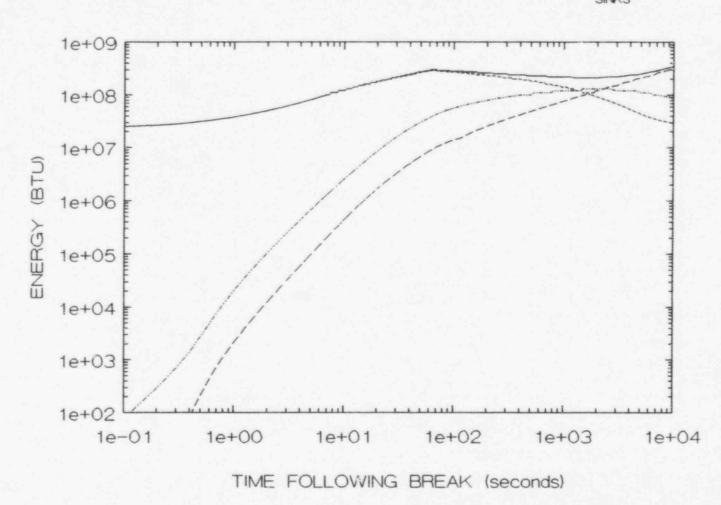
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FIGURE 2-5: ENERGY 102% POWER, 7.48 FT2 BREAK AREA ----- VAPOR TOTAL HEAT SINKS



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1e+08				
1e+07				
1e+06				The state of the s
1e+05		1		- Internal
1e+04				a - T- Municipal Control of the Cont
1e+03				
1e+02 [- 1e+0	1	1e+02	1e+03	1e+04
	Т	ME FOLLOW	ING BREAK (second	s)

FIGURE 2-6 ENERGY

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3 ASSUMPTIONS

This section presents the assumptions that are used in this calculation. The assumptions are arranged in groups which parallel the Card Series data input employed by the COPATTA Code (Reference 6.5.a).

3.1 CARD SERIES 1

a. ITEM 6: INITIAL CONTAINMENT RELATIVE HUMIDITY

The initial relative humidity inside the containment is assumed to be 60 percent. The COPATTA Code User's Manual (Reference 6.5.a, page 3-1) states that abnormal termination of the code run has been encountered when a relative humidity of 0 percent has been used, and recommends that the minimum relative humidity value should be at least 1 percent. Technically, a higher relative humidity will yield a lower peak pressure. However, the effect is small; per Table 15 of BN-TOP-3 (Reference 6.11) increasing the relative humidity from 1 percent to 100 percent will decrease the containment peak pressure by approximately 0.4 psig. Therefore, the effect of increasing the relative humidity from 1 percent to 60 percent will decrease the containment peak pressure by approximately 0.2 psig. The probability of actually having a low relative humidity of 1 percent in a closed containment with the reactor at power is remote. Experience indicates that containments tend to be hot and humid, not hot and dry. Therefore, use of a higher relative humidity of 60 percent is realistic.

b. ITEM 11: CONTAINMENT HEAT SINK REVAPORIZATION FRACTION

Since this MSLB analysis is not an equipment qualification analysis, no credit for revaporization of the heat sink condensate will be taken. Per the COPATTA Code Theory Manual (Reference 6.5.a, Appendix D, Section III.b), when the containment atmosphere is at or below the saturation temperature, all condensate formed on the heat sinks is transferred directly to the sump. When the atmosphere is superheated, revaporization allows for the condensate to be transferred to the vapor region. The introduction of the relatively cold revaporized water mass to the superheated vapor environment reduces the average energy concentration in the vapor space, and consequently reducing the containment pressure and temperature. NUREG-0588 (Reference 6.4.b, Appendix B, Section 1.b) allows for up to 8 percent of the condensate to be transferred to the vapor region during the performance of equipment qualification analyses. The assumption that no sump liquid revaporizes is conservative.

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c. ITEM 12: TOTAL PRESSURE OUTSIDE CONTAINMENT

The total pressure outside containment is assumed to be 14.7 psia. SONGS Units 2 and 3 are located at sea level. At this elevation, standard atmospheric pressure is approximately 14.7 psia per Table 3 of the ASHRAE Handbook (Reference 6.13). Per the COPATTA Code Theory Manual (Reference 6.5.a), the code uses the outside atmosphere total pressure in evaluating leakage rates between the containment and the outside environment. In this analysis no leakage is postulated and hence no leakage calculations are performed. Therefore, any outside atmosphere total pressure may be modeled with no adverse impact on the analysis results.

d. ITEM 13: RELATIVE HUMIDITY OF OUTSIDE ATMOSPHERE

The relative humidity of the outside atmosphere is assumed to be 50 percent. Per the COPATTA Code Theory Manual (Reference 6.5.a), the code uses the outside atmosphere relative humidity in evaluating leakage rates between the containment and the outside environment. In this analysis no leakage is postulated and hence no leakage calculations are performed. Therefore, any outside atmosphere relative humidity may be modeled with no adverse impact on the analysis results.

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3.2 CARD SERIES 2

a. ITEM 6: HTC BETWEEN CONTAINMENT ATMOSPHERE AND SUMP LIQUID

No heat transfer is being modeled between the sump and the vapor regions of containment; therefore, the total heat transfer coefficient (HTC) for the heat transfer between the liquid (sump) and vapor regions of the containment is assumed to be 0.0 BTU/hr-°F. A typical containment atmosphere to sump liquid HTC of 0.0 BTU/hr-°F is listed in section 3.3.1 and Table 4 of Bechtel Topical Report BN-TOP-3 (Reference 6.11). Use of this value is also recommended by Bechtel Nuclear Standard N2.3.2 (Reference 6.12, sheet 5).

The COPATTA Code uses the containment atmosphere to sump liquid HTC in evaluating heat transfer between the containment atmosphere and the sump liquid. Use of a smaller HTC is conservative because it will inhibit heat transfer from the containment air to the sump liquid, maximize containment air energy, and consequently yield higher containment pressures and temperatures.

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3.3 CARD SERIES 5

a. ITEM 2: NUMBER OF AIR COOLER TRAINS OPERATING

A review of the results presented in Calculation N-4080-007 (Reference 6.1.d) reveals that a MSLB induced peak containment pressure and temperature occurs in the event of a failure of one of the two cooling trains. The consequences of either a main steam isolation valve (MSIV) or main feedwater isolation valve (MFWIV) failure were found to be bounded by the consequences of a cooling train failure. Therefore, this MSLB analysis will assume a failure of one of the two containment cooling trains due to a single failure in the power system.

As shown on P&ID 40172A-5 (Reference 6.8.a), each train has two air coolers. Therefore, only the two air coolers of one train are assumed to be operational in this MSLB analysis.

b. ITEM 4: AIR COOLERS' SHUTOFF TIME

The air coolers will be assumed to operate for the duration of the accident as modeled in this calculation. As discussed in Design Input Item 4.1, calculations for this analysis will be terminated at 10,000 seconds.

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3.4 CARD SERIES 1001

a. ITEMS 3 and 6: TEMPERATURE OF OUTSIDE ATMOSPHERE

The outside air temperature at SONGS is assumed to be 100 °F. This temperature is conservatively greater than the normal temperatures which are noted in the SONGS Units 2&3 UFSAR (Reference 6.3.c, section 2.3.2.1.2 and Table 2.3-6). Per the UFSAR, San Onofre meteorological data taken during the years 1974 and 1975 may be considered representative of normal conditions at the site. During this two year period, the absolute maximum temperature recorded at the site was 34.3 °C (93.7 °F), occurring with an offshore Santa Ana wind on September 23, 1975.

Per the COPATIA Code Theory Manual (Reference 6.5.a, section 3.2.3), the Code uses the outside atmosphere temperature in evaluating leakage rates between the containment and the outside environment. Per the COPATTA Code User's Manual (Card Series 1001), the Code also uses the outside atmosphere temperature in initializing the outer surface temperature of the containment structure, and in evaluating heat transfer between the outer surface of the containment structure and the outside environment. In this analysis no leakage to the outside atmosphere is postulated, and hence no leakage calculations are performed. Therefore, heat transfer to the environment dictates the modeling choice.

Use of a higher air temperature is conservative because it will reduce heat transfer to the environment. Bechtel Nuclear Standard N2.3.2 (Reference 6.12, sheet 13) states that for a concrete containment structure the effect of heat transfer to the outside air is very small and virtually negligible with respect to the peak containment pressures and temperatures. However, this is true only in the short term following the onset of the accident. Long-term post-accident pressures and temperatures will be slightly maximized by maximizing the ambient temperature of the outside atmosphere.

b. ITEMS 4 and 7: HTC BETWEEN A HEAT SINK AND OUTSIDE ATMOSPHERE

The heat transfer coefficient between a heat sink and the outside atmosphere is assumed to be 2.0 BTU/hr-ft2-°F. Use of this value is recommended in Bechtel Design Standard N2.3.2 (Reference 6.12, page 13).

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4 **DESIGN INPUT**

This section presents the design inputs used in this calculation. The design inputs are arranged in groups which parallel the Card Series data input employed by the COPATTA Code.

CARD SERIES 0 4.1

a. ITEM 2: FLOW PATH THROUGH THE SDCHX

In the event of an MSLB, the source of Containment Spray System (CSS) water transfers from the Refueling Water Storage Tank to the containment sump upon receipt of a Recirculation Actuation Signal (RAS). The Shutdown Cooling Heat Exchanger (SDCHX) is used to cool containment sump water before it is recirculated through the CSS.

Calculations for this analysis will be terminated at 10,000 seconds (2.78 hours). As shown in the summary of results, this analysis termination time is sufficient to ensure determination of the peak pressure and temperature time of occurrence. By this termination time the containment pressure and temperature have also returned to near initial conditions.

If a run time in excess of 10,000 seconds were to be modeled, then the model should also reflect the Recirculation Actuation Signal (RAS) generation. Because the RAS is generated subsequent to the analysis termination time, the SDCHX will not be modeled in this MSLB accident evaluation.

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Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

Sheet No. 21

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4.2 CARD SERIES 1

a. ITEM 3: INITIAL CONTAINMENT PRESSURE

The maximum allowable containment pressure is 1.5 psig per U23 Technical Specification Limiting Condition for Operation (LCO) 3.6.1.4 (Reference 6.3.a & b). This is equivalent to a pressure of 16.2 psia (1.5 psig + 14.7 psi).

Per the COPATTA Code Theory Manual (Reference 6.5.a, section 3.1.1), the Code uses the initial containment pressure in the determination of the initial mass of air in the containment air space. The effect of varying the initial containment pressure is addressed in Bechtel Topical Report BN-TOP-3 (Reference 6.11, section 4.1.2 and Table 15). Based on the data presented in BN-TOP-3, it is concluded that maximizing the initial containment pressure will maximize the peak containment pressure. Consequently, long-term post-accident pressures will also be maximized.

b. ITEM 4: CONTAINMENT NET FREE VOLUME

The containment net free volume of 2.305e6 cubic ft is determined by Civil Calculation C-257-1.06.01 (Reference 6.1.a, page 7). This volume is conservatively based on a reduction of the containment gross volume by 110 percent of the components volume. This represents a reduction by a margin of 3.0e4 cubic ft to account for components not considered explicitly in the Civil Calculation.

Per the Copatta Code Theory Manual (Reference 6.5.a, section 3.1.1), the Code uses the containment volume in the determination of the initial masses of air and water in the containment air space. Per Bechtel Topical Report BN-TOP-3 (Reference 6.11, section 4.1.1.1), the containment volume is also used in evaluating the containment pressure, volume and energy relationship. Equations presented in Section 4.1.1.1 of BN-TOP-3 show that the containment pressure is inversely proportional to the containment volume. It is for this reason that Section 3.3.1 and Figure 16 of BN-TOP-3 recommend that the minimum containment net free volume should be modeled. Because the ideal gas law states that pressure is proportional to temperature, minimizing the containment net free volume will also maximize the peak containment temperature. Consequently, long-term post-accident pressures and temperatures will also be maximized.

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Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

Sheet No. 22

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c. ITEM 5: INITIAL CONTAINMENT TEMPERATURE

The initial bulk average containment atmosphere temperature is 120 °F. Technical Specification LCO 3.6.1.5 (References 6.3.a & b) indicates that this is the maximum allowable bulk average containment temperature.

Per the COPATTA Code Theory Manual (Reference 6.5.a, section 3.1.1), the Code uses the initial containment temperature in the determination of the initial mass of air in the containment air space. Per sections 3.1.2 and A.3 of the COPATTA Code Theory Manual, the Code also uses the initial containment temperature in the determination of the initial temperature profiles of those heat sinks in contact with the containment air.

The effect of varying the initial containment temperature is addressed in Bechtel Topical Report BN-TOP-3 (Reference 6.11, section 4.1.2 and Table 15). Based on the data presented, it is concluded that maximizing the initial containment temperature will maximize both the peak containment pressure and temperature. This conclusion is consistent with the fact that maximizing the initial containment temperature will increase the initial heat sink temperatures, thereby minimizing the effectiveness of the larger structural heat sinks in removing energy from the containment air space. Consequently, long-term post-accident pressures and temperatures will also be maximized.

d. ITEM 8: INITIAL AVERAGE REACTOR COOLANT TEMPERATURE

CE Letter S-CE-2604 (Reference 6.2.a) provides the mass and energy release data to be modeled for the LOCA and MSLB scenarios. Appendix H to this CE Letter indicates that an initial average (reactor) coolant temperature of 582.945 °F should be modeled in the containment pressure-temperature analyses. This temperature is similar to the 582.1 °F average Reactor Vessel operating temperature specified in the RCS System Description SD-SO23-360 (Reference 6.7.a, section 2.2.1).

This parameter is used to set the initial temperature of all heat conducting region surfaces in contact with the reactor coolant. Since no heat sinks in contact with the reactor coolant are explicitly modeled in this analysis, the average reactor coolant temperature is not actually used in the COPATTA calculation.

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Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

Sheet No. 23

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CARD SERIES 5 4.3

a. ITEM 3: TIME OF AIR COOLER INITIATION

Sheet 6 of Calculation N-4080-003 (Reference 6.1.h) indicates that the emergency fan coolers (EFCs) will start 15 seconds after the onset of a MSLB event with offsite power available. Sheet 6 of the analysis presented in Reference 6.1.h notes that this result is specifically applicable to a DBA MSLB (steam line break at 102% power), and the containment high pressure setpoint is currently 5 psig. Sheet 24 of Reference 6.1.h gives a time line for emergency fan cooler operation following the DBA MSLB.

Of note is that the air cooler initiation time modeled in Calculation N-4080-003 is based on two seconds required for the containment pressure to increase to the containment high pressure setpoint of 5.0 psig. Per the results of this calculation, the setpoint pressure of 5.0 psig is reached in less than one second. The difference between the modeled time of occurrence and the actual time of occurrence represents an additional one second of margin in this analysis.

Another conservatism present in the 15 second EFC start time is the availability of the component cooling water (CCW) to the fan cooler. Per sheet 21 of Reference 6.1.h, the CCW block valves will be 83% open at the time the EFCs reach full speed (13 seconds), but the air cooler start time is conservatively modeled as the time at which the CCW block valves are fully opened. The CCW block valves will be passing nearly full flow to the emergency fan coolers for two seconds prior to the assumed 15 second start time; therefore, an additional safety margin is added by a 15 second EFC start time.

Delaying the start of the containment air cooler operation conservatively delays the removal of containment atmosphere energy via the air coolers, thereby maintaining a larger containment air energy inventory that will maximize the containment pressures and temperatures.

b. ITEM 8: TEMPERATURE OF AIR COOLER HEAT EXCHANGER COOLANT

The air cooler heat exchanger coolant temperature is 105 °F. The maximum inlet temperature of the air cooler HX coolant is no greater than the maximum Component Cooling Water System (CCWS) heat exchanger outlet temperature. Per CCWS Design Basis Document DBD-SO23-400 (Reference 6.6.a, Table 0-1) and Calculation M-0026-001 (Reference 6.1.c, page 6), the maximum CCWS heat exchanger outlet temperature is 105 °F.

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Temperature changes in the uninsulated component cooling water lines between the CCWS heat exchanger outlet and the air coolers are assumed negligible.

Maximizing the air cooler coolant temperature minimizes the heat removed from the containment air circulating through the air cooler, thereby yielding a larger containment air energy inventory that will maximize the containment pressures and temperatures.

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4.4 CARD SERIES 301

Card Series 301 is a table that is used to input blowdown following pipe rupture. It provides the water addition rate and the enthalpy of the water at various times. The NSSS vendor determines the mass and energy release data that describes a spectrum of break types and break sizes. This "blowdown" data is introduced into the containment air space where it serves to increase both the containment pressure and temperature. Increasing the total mass and energy release will increase the containment pressure and temperature response.

The conclusions presented in Calculation N-4080-007 (Reference 6.1.d) indicate that the worst case MSLB is a 7.4765 ft2 break area at 102 percent power, and a failure of a single cooling train with offsite power available. The mass and energy release data for this worst case MSLB is documented in C-E Letter S-CE-4007 (Reference 6.2.b, Appendix A). C-E Letter S-CE-2604 (Reference 6.2.a) mentions that the availability of offsite power permits continued reactor coolant pump flow. Maintaining reactor coolant pump flow maximizes the rate of primary to secondary heat transfer which maximizes the rate of mass/energy release.

MSLB mass flow rates in C-E Letter S-CE-4007 are presented in units of pounds per second. The water addition rates entered into Card Series 301 are in units of pounds per hour. As shown in the following table, the Card Series 301 input data were calculated by scaling the CE break mass flow rates by the conversion factor of 3600 seconds per hour.

MSLB energy flow rates in C-E Letter S-CE-4007 are presented in units of Million BTU per second. The water enthalpies entered into Card Series 301 are in units of BTU per pound. As shown in the following table, the Card Series 301 input data were calculated by dividing the CE energy flow rates by the CE mass flow rates at each time step, and then multiplying by the conversion factor of 1 × 106 BTU per Million BTU.

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MAIN STEAM LINE BREAK MASS AND ENERGY RELEASE DATA (a) (7.4765 ft² break area, 102 percent power, cooling train failure)

TIME CS 301, Item 1	NSSS SUPPI (C-E Letter Reference	S-CE-4007,		NVERTED FOR C Series 301, Items 2	The same of the sa
	BREAK MASS FLOW RATE	BREAK ENERGY FLOW RATE	BREAK MASS FLOW RATE	BREAK ENTHALPY	BREAK ENERGY FLOW RATE
(sec)	(lbm/sec)	(10 ⁶ BTU/sec)	(lbm/hour)	(BTU/lbm)	(BTU/hr)
0	14293.11	17.088682	5.145520E7	1.195589E3	6.151926E10
0.22	13525.09	16.196053	4.869032E7	1.197482E3	5.830579E10
0.42	12839.54	15.387747	4.622234E7	1.198466E3	5.539589E10
0.62	12238.71	14.679232	4 405936E7	1.199410E3	5.284524E10
1.08	11120.21	13.361993	4.003276E7	1.201595E3	4.810317E10
1.58	10246.82	12.314189	3.688855E7	1.201757E3	4.433108E10
2.08	9572.14	11.505884	3.445970E7	1.202018E3	4.142118E10
2.58	9239.69	11.096741	3.326288E7	1.200986E3	3.994827E10
3.58	8757.24	10.517954	3.152606E7	1.201058E3	3.786463E10
4.58	8412.41	10.108812	3.028468E7	1.201655E3	3.639172E10
5.58	8166.89	9.809439	2.940080E7	1.201123E3	3.531398E10
6.58	7985.75	9.591895	2.874870E7	1.201126E3	3.453082E10
7.58	7518.26	9.055021	2.706574E7	1.204404E3	3.259808E10
8.58	6856.46	8.257692	2.468326E7	1.204367E3	2.972769E10
9.58	6374.91	7.676909	2.294968E7	1.204238E3	2.763687E10
10.58	6000.34	7.223859	2.160122E7	1.203908E3	2.600589E10
12.58	5397.62	6.494388	1.943143E7	1.203195E3	2.337980E10
14.58	4905.39	5.897638	1.765940E7	1.202277E3	2.123150E10
16.58	4547.89	5.464546	1.637240E7	1.201556E3	1.967237E10
18.58	4290.89	5.153199	1.544720E7	1.200963E3	1.855152E10
20.58	4092.48	4.912703	1.473293E7	1.200422E3	1.768573E10

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Sheet No. 27

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MAIN STEAM LINE BREAK MASS AND ENERGY RELEASE DATA (a) (7.4765 ft² break area, 102 percent power, cooling train failure)

TIME CS 301, Item 1	NSSS SUPPL (C-E Letter S Reference	S-CE-4007,		NVERTED FOR Conserved Series 301, Items 2	
(sec)	BREAK MASS FLOW RATE (lbm/sec)	BREAK ENERGY FLOW RATE (106 BTU/sec)	BREAK MASS FLOW RATE (lbm/hour)	BREAK ENTHALPY (BTU/lbm)	BREAK ENERGY FLOW RATE (BTU/hr)
25.58	3687.57	4.420734	1.327525E7	1.198820E3	1.591464E10
30.58	3394.05	4.065479	1.221858E7	1.197825E3	1.463572E10
35.58	3184.46	3.811012	1.146406E7	1.196753E3	1.371964E10
40.58	2942.03	3.516629	1.059131E7	1.195307E3	1.265986E10
45.58	2722.56	3.251185	9.801216E6	1.194165E3	1.170427E10
50.58	2536.83	3.026656	9.132588E6	1.193086E3	1.089596E10
60.58	2300.09	2.739258	8.280324E6	1.190935E3	9.861329E9
61.08	2012.66	2.396976	7.245576E6	1.190949E3	8.629114E9
62.08	1612.04	1.916982	5.803344E6	1.189165E3	6.901135E9
62.58	899.64	1.065766	3.238704E6	1.184658E3	3.836758E9
64.58	109.69	0.129429	3.948840E5	1.179953E3	4.659444E8
68.58	29.84	0.037332	1.074240E5	1.251072E3	1.343952E8
71.08	0	0	0	0	0
2E7	0	0	0	0	0

a. The mass and energy release rates are assumed to vary linearly between each data point.

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4.5 CARD SERIES 801

a. INJECTION MODE CHARACTERISTICS

The results presented in Calculation N-4080-007 indicates that the MSLB induced peak containment pressure and temperatures occur for the circumstance of a failure of one of the two cooling trains. The consequences of either a MSIV or MFWIV failure were found to be bounded by the consequences of a cooling train failure.

a. 1 Injection Mode Start Times

a.1.(a) Containment Spray System Injection Mode Start Time

With offsite power available, the containment spray is functional within 49 seconds per Calculation N-4080-003 (Reference 6.1.h, sheet 6). To provide margin to address any future changes in system performance, this analysis assumes that the time of containment spray initiation with offsite power available is 50 seconds.

Delaying the start of the containment spray system operation conservatively delays the removal of containment atmosphere energy via the CSS, thereby maintaining a larger containment air energy inventory that will increase the maximum containment pressure and temperature.

a.1.(b) Safety Injection System Injection Mode Start Time

The Safety Injection System (SIS) supplies water to the reactor via pressurized discharge from the Safety Injection Tanks (SITs) as well as via pumped flow from the Refueling Water Storage Tank (RWST) upon receipt of a Safety Injection Actuation Signal (SIAS). Per the ESFAS System Description (Reference 6.7.d, Section 2.1.2.1.1), a SIAS is generated upon receipt of two out of four low pressurizer pressures or a high containment pressure.

Because no rupture of the primary system exists in the MSLB event, the mass of water added to the Reactor Coolant System by the Safety Injection System (SIS) is only to compensate for inventory shrinkage due to the rapid cooldown. The effect of the safety injection on the mass release into containment is therefore implicitly modeled by Combustion Engineering in C-E Letter S-CE-4007, and not modeled in this calculation.

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a.2 Injection Mode Flow Rates

a.2.(a) Containment Spray System Injection Mode Flow Rate

A CSS injection mode volumetric flow rate of 1612 gallons/minute will be modeled beginning at the time that a full flow spray pattern is initiated at the spray nozzles, and continuing until the recirculation mode begins. This flow rate of 1612 gallons/minute represents the minimum CSS injection mode flow rate, and is calculated in M-0014-009 (Reference 6.1.b). This flow rate is for the conditions of a CSS Pump degradation of 7.5 percent, a containment peak pressure of 60 psig, and a minimum RWST water level of 33.35 feet.

Minimizing the CSS injection mode flow rate reduces the amount of spray water available to remove energy from the containment air space, thereby maximizing the containment pressures and temperatures.

At an injection mode water temperature of 100 °F (see following discussion), the containment spray flow rate of 1612 gallons/minute has a specific volume of 0.016130 ft3/pound (Reference 6.14, page 88), and will be modeled in Card Series 801 with a mass flow rate of:

 $\dot{M} = [(1612 \text{ gallons/minu}) \div (0.016130 \text{ ft}^3/\text{lbm})] \times (0.13368 \text{ ft}^3/\text{gallon}) \times (60 \text{ min/hour})$ $\dot{M} = 8.02e5 \text{ pounds/hour}$

a.3 Injection Mode Water Temperature/Source

The SIS and CSS initially draw water from the RWST upon receipt of a SIAS, and subsequently from the Containment Sump upon receipt of a Recirculation Actuation Signal (RAS). Technical Specification LCO 3.5.4(c) (References 6. 3.a & b) indicates that the maximum allowable RWST temperature is 100 °F. It is assumed that the SIS and CSS flow during the Injection Mode is at this maximum allowable RWST temperature of 100 °F.

Maximizing the RWST water temperature increases the CSS injection mode water droplet temperature. Increasing the spray droplet water temperature reduces the ability of the spray droplets to remove energy from the containment air space, thereby maximizing the containment pressures and temperatures.

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b. RECIRCULATION MODE CHARACTERISTICS

b.1 Recirculation Mode Start Time

The Recirculation Actuation Signal (RAS) is designed to change suction of the HPSI and CS pumps from the RWST to the Containment Emergency Sump when the RWST level is low.

The source of CSS and SIS water transfers from the RWST to the containment sump upon receipt of a RAS. Per the ESFAS System Description (Reference 6.7.d, section 2.1.2.1.7), an RAS is generated upon receipt of two out of four RWST low level signals. During the injection mode the RWST water is discharged in the form of containment spray, safety injection, and charging flow. To determine the time of CSS and SIS recirculation mode initiation it is necessary to quantify the useable RWST water volume, the flow rates exiting the RWST during the injection mode, and the time that these flow rates begin their injection mode discharge.

The useful RWST volume is modeled as 300,000 gallons. CE Letter S-CE-6814 (Reference 6.2.c) states that the volume required for injection is 313,706 gallons when instrument error of the RWST low level setpoint and the RAS setpoint are considered, and 300,000 gallons when this instrument error is not considered. In this calculation, the RWST volume is minimized to hasten the start of the recirculation mode.

$$V_{RWST}$$
 = 300000 gallons
= [(1612 gpm) × (t_{recirc} - 50 sec) / (60 sec/min)]

 $t_{recirc} = 1.12E4$ seconds

Operation of the High Pressure Safety Injection (HPSI) pumps will also drain the RWST. During the MSLB event, the RCS is maintained at a pressure that is sufficiently high to preclude the delivery of any HPSI flow into the RCS other than that which is necessary to compensate for RCS shrinkage during cooldown. The RWST inventory used by the SIS for RCS shrinkage compensation is minimal and will not significantly reduce the estimated 11,000 second drain time of the RWST.

The time of occurrence of peak containment pressure and temperature is dependent on the start f the CSS injection mode, however the time for CSS recirculation mode initiation will have no ampact on the containment peak pressure or temperature for an MSLB. Since the time for the recirculation mode is greater than the analyses run time, CSS recirculation will not be modeled in this MSLB analysis.

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CARD SERIES 1101 4.6

a. ITEMS 5 and 6

The air cooler heat removal rate as a function of containment atmosphere saturation temperature is determined in Calculation M-0072-036 (Reference 6.1.e) for the conditions of a CCWS volumetric flow rate at the inlet to a containment emergency air cooler of 2000 gallons/minute at 105 °F, a constant air flow rate through the air cooler of 31000 ft³/minute, and a water side fouling factor of 5×10^4 . The air cooler duty curve determined in Calculation M-0072-036 is plotted and tabulated on sheets 8 and 10 of that calculation.

The air cooler duty curve determined in Calculation M-0072-036 includes performance data for a superheated containment condition when the containment atmosphere saturation temperature exceeds 300 °F (corresponding to a containment atmosphere saturation pressure of 67 psia). The COPATTA Code requires air cooler data for saturated conditions only. Since the containment peak saturation temperature determined by previous MSLB P/T is below 300 °F, data for conditions above 300 °F is considered irrelevant for this calculation.

Card Series 1101 is entered in the input data file as shown in the following table. As an initialization point, when the containment air temperature is equivalent to the CCW temperature of 105 °F at the inlet to the air cooler, then the air cooler will not remove any heat from the containment air.

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CONTAINMENT AIR COOLER ABILITY TO REMOVE AIR ENERGY

CONTAINMENT ATMOSPHERE SATURATION TEMPERATURE (Calc M-0072-036, pg 10) Card Series 1101, Item 5 (°F)	AIR COOLER HEAT REMOVAL RATE Card Seriec 1101, Item 6 (BTU/hour)	CONTAINMENT ATMOSPHERE CONDITIONS
105	0.000	Initial Condition
120	1.670e+06	Saturated Condition
130	3.020e+06	Saturated Condition
140	4.570e+06	Saturated Condition
150	6.320e+06	Saturated Condition
160	8.270e+06	Saturated Condition
170	1.040e+07	Saturated Condition
180	1.273e+07	Saturated Condition
190	1.523e+07	Saturated Condition
200	1.788e+07	Saturated Condition
210	2.068e+07	Saturated Condition
220	2.361e+07	Saturated Condition
230	2.664e+07	Saturated Condition
240	2.974e+07	Saturated Condition
250	3.291e+07	Saturated Condition
260	3.611e+07	Saturated Condition
270	3.931e+07	Saturated Condition
280	4.252e+07	Saturated Condition
287	4.474e+07	Saturated Conditions
290	4.569e+07	Saturated Condition
300	4.882e+07	Saturated Condition
≥ 320	N/A	Superheated Condition

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4.7 CARD SERIES 1201

a. ITEMS 2 and 3

Containment spray heat transfer efficiency varies as a function of the ratio of water vapor to air mass in the containment atmosphere. Data points listed in the following table are extracted from Bechtel Topical Report BN-TOP-3 (Reference 6.11, Revision 4, Section 3.2.6 and Figure 2). Per BN-TOP-3, this data is for a spray system with a mean spray drop diameter of 1000 microns and a drop fall height of 20 feet, and is standard "for virtually all PWR containment analyses".

Per the UFSAR (Reference 6.3.c, Section 6.2.2.1.2.2.B), the SONGS Units 2&3 mean spray droplet diameter is about 650 microns. Since efficiency is inversely proportional to the diameter, use of spray heat transfer efficiency data applicable to a larger spray drop diameter is conservative. Decreasing the CSS efficiency reduces the ability of the spray droplets to remove energy from the containment air space, thereby maximizing the containment pressures and temperatures.

CONTAINMENT SPRAY SYSTEM HEAT TRANSFER EFFICIENCY (mean spray drop diameter of 1000 microns and a drop fall height of 20 feet

STEAM TO AIR MASS RATIO Card Series 1201, kem 2 (unitless)	SPRAY EFFICIENCY Card Series 1201, Item 3 (percent)
0.0	72.9
0.1	73.7
0.2	74.7
0.3	75.7
0.4	77.1
0.5	78.8
0.6	80.9
0.7	83.2
0.8	86.3
0.9	91.2
1.0	96.1
1.1	98.3
1.2	99.5
1.3	100.0

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4.8 HEAT SINK DATA SERIES

A fundamental change in this p/t analysis involves the use of the Uchida concensing heat transfer correlation. BN-TOP-3 (Reference 6.11) page 3-12 indicates that the condensing heat transfer correlation used in main steam line break analysis is the Uchida correlation. This modification represents a deviation from the Modified Tagami heat transfer coefficient used in previous MSLB analyses. The COPATIA User's Manual, page 3-55 also indicates that the Uchida HTC is typically used for MSLB analysis.

The change from a Modified Tagami HTC to a Uchida HTC is required as one step in the resolution of Open Item Report 92-069 (Reference 6.9.f)

a. CONTAINMENT LINER/CONCRETE AIR GAP INTERFACE

In this analysis the effective thickness of the interface (air gap) will be modeled as 0.00035 feet. This value is based on a containment liner to containment concrete interface conductance of 50 BTU/hr-ft²-°F, and an air thermal conductivity of 0.0174 BTU/hr-ft-°F.

A typical containment liner to containment concrete interface conductance of 50 BTU/hr-ft²-°F will be modeled. This conductance of 50 BTU/hr-ft2-°F is listed in Bechtel Topical Report BN-TOP-3 (Reference 6.11, Section 3.3.1 and Table 4). Appendix A of BN-TOP-3 (page A-4) indicates that an effective one-dimensional interface conductance of this value will ensure a conservative estimate of heat transfer to the containment wall. There will be some resistance to heat transfer from the containment atmosphere to the containment structure at the containment liner-concrete interface due to air gaps or voids between the liner and the concrete. This resistance is accounted for in this interface conductance. Use of a smaller interface conductance is conservative because it will inhibit heat transfer from the containment air to the containment concrete walls, maximize containment air energy, and consequently yield higher containment pressures and temperatures.

At a long-term average post-accident containment air temperature of 200 °F, Engineering Heat Transfer (Reference 6.15, Table A-6, page 577) indicates that the air thermal conductivity is 0.0174 BTU/hr-ft-°F. The thermal conductivity of a material is a measure of the material's ability to conduct heat. Minimizing a heat sink's thermal conductivity will inhibit heat transfer from the containment air to the heat sinks. During the early pass of an accident this will maximize containment air energy, and consequently yield higher containment pressures and temperatures.

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Based on a containment liner to containment concrete interface conductance (h) of 50 BTU/hr-ft²-°F, and an air thermal conductivity (k) of 0.0174 BTU/hr-ft-°F, the effective thickness of the interface (air gap) will be:

Interface thickness, $\Delta t = (0.0174 \text{ BTU/hr-ft}^{\circ}\text{F}) \div (50 \text{ BTU/hr-ft}^{2}^{\circ}\text{F})$ Interface thickness, $\Delta t = 0.00035$ feet

b. HS #1 - REACTOR BUILDING DOME

The characteristics of the Reactor Building Dome are as determined in Calculation N-4080-002 (Reference 6.1.g, pages 121 through 125) for Heat Sink 1, except for the thickness of the Containment Liner/Concrete air gap interface.

The thickness of the Containment Liner/Concrete air gap interface is modified to address a change in the containment liner to containment concrete interface conductance, as discussed in Design Input Item 13.a.

c. HS #2 - REACTOR BUILDING CYLINDER #1 (ABOVE GRADE, BETWEEN EL. 29'6" AND 112'0")

The characteristics of the Reactor Building Cylinder #1 (above grade, between plant elevations 29'6" and 112'0") are as determined in Calculation N-4080-002 (pages 125 through 128) for Heat Sink 2, except for the thickness of the Containment Liner/Concrete air gap interface.

The thickness of the Containment Liner/Concrete air gap interface is modified to address a change in the containment liner to containment concrete interface conductance, as discussed in Design Input Item 13.a.

d. HS #3 - REACTOR BUILDING CYLINDER #2 (BELOW GRADE, BETWEEN EL. 15'0" AND 29'6")

The characteristics of the Reactor Building Cylinder #2 (below grade, between plant elevations 15'0" and 29'6") are as determined in Calculation N-4080-002 (pages 134 through 136) for Heat Sink 3, except for the thickness of the Containment Liner/Concrete air gap interface.

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The thickness of the Containment Liner/Concrete air gap interface is modified to address a change in the containment liner to containment concrete interface conductance, as discussed in Design Input Item 13.a.

e. HS #4 - BASEMAT (OTHER THAN THE REACTOR BASEMAT)

The characteristics of the Basemat (other than the Reactor Basemat) are as determined in Calculation N-4080-002 (pages 137 through 139) for Heat Sink 4.

f. HS #5 - REACTOR BASEMAT AND STEAM GENERATOR PEDESTALS

The characteristics of the Reactor Basemat and Steam Generator Pedestals are as determined in Calculation N-4080-002 (pages 139 through 141) for Heat Sink 5.

g. HS #6 - REACTOR CAVITY WALLS BELOW EL. 15'0"

The characteristics of the Reactor Cavity Walls below plant elevation 15'0" are as determined in Calculation N-4080-002 (pages 142 through 144) for Heat Sink 6.

h. HS #7 - REACTOR CAVITY WALLS ABOVE EL. 15'0"

The characteristics of the Reactor Cavity Walls above plant elevation 15'0" are as determined in Calculation N-4080-002 (pages 144 through 146) for Heat Sink 7.

i. HS #8 - LINED REFUELING CANAL WALLS

The characteristics of the Lined Refueling Canal Walls are as determined in Calculation N-4080-002 (pages 146 through 149) for Heat Sink 8.

 HS #9 - STEAM GENERATOR COMPARTMENT WALLS, UNLINED REFUELING CANAL WALLS ABOVE EL. 63'6", AND OTHER INTERIOR WALLS

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The characteristics of the Steam Generator Compartment Walls, Unlined Refueling Canal Walls above plant elevation 63'6", and Other Interior Walls are as determined in Calculation N-4080-002 (pages 149 through 152) for Heat Sink 9.

k. HS #10 - FLOOR SLABS (OTHER THAN BASEMATS)

The characteristics of the Floor Slabs (other than basemats) represent a refinement of the characteristics of determined in Calculation N-4080-002 (pages 152 through 155) for Heat Sink 10.

A review of Calculation N-4080-002 (page 153) indicates that the concrete thickness of the floor slabs is 1.5 feet, and is based on input data provided as Attachment 1 to Calculation N-4080-002 (page 327). When the nodalization of the Concrete Region was performed, Calculation N-4080-002 (page 153) modeled the concrete as Heat Sink 10 Regions 3, 4 and 5, with a total concrete thickness of 2.0 feet. To model the correct concrete thickness requires that the Region 5 thickness be reduced by 0.5 feet.

1. HS #11 - LIFTING DEVICES (EXCEPT STAINLESS STEEL PARTS)

The characteristics of the Lifting Devices (except stainless steel parts) are as determined in Calculation N-4080-005 (Reference 6.1.f, pages 42 through 44) for Heat Sink 10. This heat sink description represents a refinement of the characteristics of the Lifting Devices first determined in Calculation N-4080-002 (pages 156 through 158) for Heat Sink 11.

m. HS #12 - MISCELLANEOUS CARBON STEEL (WITH THICKNESS GREATER THAN 2.50 IN)

The characteristics of the Miscellaneous Carbon Steel (with thickness greater than 2.50 in) are as determined in Calculation N-4080-005 (pages 44 through 47) for Heat Sink 11. This heat sink description represents a refinement of the characteristics of the Miscellaneous Carbon Steel first determined in Calculation N-4080-002 (pages 158 through 161) for Heat Sink 12.

n. HS #13 - MISCELLANEOUS CARBON STEEL (WITH THICKNESS BETWEEN 1.00 IN AND 2.50 IN)

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The characteristics of the Miscellaneous Carbon Steel (with thickness between 1.00 in and 2.50 in) are as determined in Calculation N-4080-005 (pages 47 through 50) for Heat Sink 12. This heat sink description represents a refinement of the characteristics of the Miscellaneous Carbon Steel first determined in Calculation N-4080-002 (pages 161 through 165) for Heat Sink 13.

o. HS #14 - MISCELLANEOUS CARBON STEEL (WITH THICKNESS BETWEEN 0.50 IN AND 1.00 IN)

The characteristics of the Miscellaneous Carbon Steel (with thickness between 0.50 in and 1.00 in) are as determined in Calculation N-4080-005 (pages 50 through 54) for Heat Sink 13. This heat sink description represents a refinement of the characteristics of the Miscellaneous Carbon Steel first determined in Calculation N-4080-002 (pages 165 through 169) for Heat Sink 14.

p. HS #15 - MISCELLANEOUS CARBON STEEL (WITH THICKNESS LESS THAN 0.50 IN)

The characteristics of the Miscellaneous Carbon Steel (with thickness less than 0.50 in) are as determined in Calculation N-4080-005 (pages 54 through 59) for Heat Sink 14. This heat sink description represents a refinement of the characteristics of the Miscellaneous Carbon Steel first determined in Calculation N-4080 302 (pages 169 through 173) for Heat Sink 15.

q. HS #16 - ELECTRICAL EQUIPMENT

The characteristics of the Electrical Equipment are as determined in Calculation N-4080-005 (pages 59 through 61) for Heat Sink 15. This heat sink description represents a refinement of the characteristics of the Electrical Steel first determined in Calculation N-4080-002 (pages 174 through 176) for Heat Sink 16.

r. HS #17 - MISCELLANEOUS STAINLESS STEEL

The characteristics of the Miscellaneous Stainless Steel are as determined in Calculation N-4080-005 (pages 62 through 65) for Heat Sink 16. This heat sink description represents a refinement of the characteristics of the Miscellaneous Stainless Steel as first determined in Calculation N-4080-002 (pages 176 through 179) for Heat Sink 17.

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s. HS #18 - UNLINED REFUELING CANAL WALLS (BELOW EL. 63'6")

The characteristics of the Unlined Refueling Canal Walls (below plant elevation 63'6") are as determined in Calculation N-4080-002 (pages 180 through 182) for Heat Sink 18.

t. HS #19 - REACTOR BUILDING CYLINDER #3 (THE CONTAINMENT SECTION WITH EMBEDDED STIFFENERS BETWEEN EL. 29'6" AND 112'0")

The characteristics of the Reactor Building Cylinder #3 (the Containment Section with Embedded Stiffeners between plant elevations 25'6" and 112'0") are as determined in Calculation N-4080-002 (pages 183 through 189) for Heat Sink 19, except for the thickness of the Containment Liner/Concrete air gap interface, and except for the thickness of the concrete layer.

The thickness of the Containment Liner/Concrete air gap interface is modified to address a change in the containment liner to containment concrete interface conductance, as discussed in Design Input Item 13.a.

Due to an addition error, Calculation N-4080-002 (page 188) improperly modeled the concrete layer as 3.56524 feet thick. In this analysis the concrete layer will be modeled as 4.21108 feet, corresponding to the average thickness that was actually determined in Calculation N-4080-002 (page 186).

u. HS #20 - VENT TUNNELS

The characteristics of the Vent Tunnels are as determined in Calculation N-4080-002 (pages 190 through 192) for Heat Sink 20.

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14 CARD SERIES 410001: MATERIAL PROPERTIES

This Card Series provides the thermal conductivity and the volumetric heat capacity of the material used in this analysis. Five materials are utilized by this analysis:

Material 1 Carbon Steel

Material 2

Concrete

Material 3

Stainless Steel

Material 4 Organic Paint Coating

Material 5

Air Gap

The thermal conductivity of a material is a measure of the material's ability to conduct heat. Minimizing a heat sink's thermal conductivity will inhibit heat transfer from the containment air to the heat sinks. During the early part of an accident this will maximize containment air energy, and consequently yield higher containment pressures and temperatures.

The volumetric heat capacity of a material is a measure of the material's ability to store energy. Minimizing a heat sink's volumetric heat capacity will inhibit heat retention by the heat sink, and consequently maximize energy retention within the containment air. This will yield higher containment pressures and temperatures.

a. ITEMS 2 and 3: CARBON STEEL

A typical Carbon Steel thermal conductivity of 25 BTU/hr-ft-°F is listed in Bechtel Topical Report BN-TOP-3 (Reference 6.11, Section 3.3.1 and Table 4). Use of this value is recommended by Bechtel Nuclear Standard N2.3.2 (Reference 6.12, sheet 14).

A typical Carbon Steel Volumetric Heat Capacity of 54 BTU/ft3-°F is listed in Bechtel Topical Report BN-TOP-3 (Section 3.3.1 and Table 4). Use of this value is recommended by Bechtel Nuclear Standard N2.3.2 (sheet 14).

b. ITEMS 4 and 5: CONCRETE

A typical Concrete thermal conductivity of 0.8 BTU/hr-ft-°F is listed in Bechtel Topical Report BN-TOP-3 (Reference 6.11, Section 3.3 1 and Table 4). Use of this value is recommended by Bechtel Nuclear Standard N2.3.2 (Reference 6.12, sheet 14).

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A typical Concrete Volumetric Heat Capacity of 30 BTU/ft3-°F is listed in Bechtel Topical Report BN-TOP-3 (Section 3.3.1 and Table 4). Use of this value is recommended by Bechtel Nuclear Standard N2.3.2 (sheet 14).

c. ITEMS 6 and 7: STAINLESS STEEL

A typical Stainless Steel thermal conductivity of 10 BTU/hr-ft- F is listed in Bechtel Topical Report BN-TOP-3 (Reference 6.11, Section 3.3.1 and Table 4). This value is typical for Types 304 and 316 austenitic stainless steel used for inside containment SS piping. Use of a value of 10 BTU/hr-ft-°F is recommended by Bechtel Nuclear Standard N2.3.2 (Reference 6.12, sheet 14).

A typical Stainless Steel Volumetric Heat Capacity of 54 BTU/ft3-°F is listed in Bechtel Topical Report BN-TOP-3 (Section 3.3.1 and Table 4). Use of this value is recommended by Bechtel Nuclear Standard N2.3.2 (sheet 14).

d. ITEMS 8 and 9: ORGANIC PAINT COATING

A typical Organic Paint thermal conductivity of 0.1 BTU/hr-ft-°F is listed in Bechtel Topical Report BN-TOP-3 (Reference 6.11, Section 3.3.1 and Table 4). Use of this value is recommended by Bechtel Nuclear Standard N2.3.2 (Reference 6.12, sheet 14).

A typical Organic Paint Volumetric Heat Capacity of 20 BTU/ft3-°F is listed in Bechtel Topical Report BN-TOP-3 (Section 3.3.1 and Table 4). Use of this value is recommended by Bechtel Nuclear Standard N2.3.2 (sheet 14).

e. ITEMS 10 and 11: AIR GAP (@ 200 °F)

At a long-term average post-accident containment air temperature of 200 °F, the book Engineering Heat Transfer, by S.T. Hsu, (Reference 6.15, Table A-6, page 577) indicates that the air thermal conductivity is 0.0174 BTU/hr-ft-°F.

The volumetric heat capacity is equal to the product of the air density (p) and the specific heat of air at constant volume (C_v). The air specific heat capacity at constant volume rather than at constant pressure (Co) is employed because the containment air pressure is not constant, it varies greatly during the course of the accident. However, the air volume of the heat sinks is constant. The specific heat of air at constant volume is equal to the product of the specific heat of air at

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constant pressure and the ratio of specific heats ($k = C_p/C_v$). At a long-term average post-accident containment air temperature of 200 °F, the book Engineering Heat Transfer, by S.T. Hsu, (Table A-6, page 577) indicates that ρ is equal to 0.060 lbm/ft³, and C_p is equal to 0.241 BTU/lbm-°F. Crane Technical Paper 410 (Reference 6.10, page A-22) indicates that k is equal to 1.4. Therefore, the air volumetric heat capacity is:

$$\rho C_v = (0.060 \text{ lbm/ft}^3) \times (0.241 \text{ BTU/lbm-}^\circ\text{F}) \div (1.4)$$

 $\rho C_v = 0.0103 \text{ BTU/ft}^3\text{-}^\circ\text{F}$

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5 METHODOLOGY

The MSLB case evaluated in this calculation is a 7.48 ft² steam break at 102% power with offsite power available and a loss of one of two cooling trains. The evaluations utilized the Bechtel COPATTA computer code (Reference 6.5.a) model the containment response to the MSLB.

The COPATTA Code is capable of considering the effects of reactor system blowdown, core decay power energy release, metal-water reaction energy release, and sensible heat release from the reactor system piping. In addition, the Code can consider heat absorption by the containment structure and equipment within the structure, and engineered safeguard features including air coolers, containment sprays, and reactor core safety injection.

The COPATTA Code calculates conditions in two separate regions of the containment: the containment atmosphere (vapor region), and the sump (liquid region). Following completion of the primary system blowdown, the program also calculates conditions in a third region, the water contained in the reactor vessel. The three regions are open systems in a thermodynamic sense since the COPATTA Code permits mass flow across the boundaries of all three regions. Mass and energy are transferred between the liquid and vapor regions by boiling, condensation, or liquid dropout. Each region is assumed homogeneous, but a temperature difference can exist between regions. Any moisture condensed in the vapor region during a time increment is assumed to fall immediately into the liquid region. Non-condensible gases are included in the vapor region.

This analysis with the COPATTA Code is presented in four sections:

Section 8.1: COPATTA Code Card Series Input Data

Section 8.2: COPATTA Code Input Files Section 8.3: COPATTA Code Output

Section 8.4: Mass and Energy Balance

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REFERENCES

6.1 Calculations

- a. SONGS Units 2&3 Calculation C-257-1.06.01, Revision 1, "Containment Shell Analysis - Containment Passive Heat Sink" (dated 7/28/77).
- b. SONGS Units 2&3 Calculation M-0014-009, Revision 0, "Containment Spray Pumps In Service Testing Minimum Requirements". (dated 3/3/93) PB 94
- c. SONGS Units 2&3 Calculation M-0026-001, Revision 5, "Component Cooling Water Heat Exchangers" (dated 11/15/89).
- d. SONGS Units 2&3 Calculation N-4080-007, Revision 2, "Containment Pressure and Temperature From MSLB at Various Power Levels" (dated 4/21/83)
- e. SONGS Units 2&3 Calculation M-0072-036, Revision 0, "Containment Emergency Cooler Performance Verification". (dated 12/9/93) 131-10-94
- f. SONGS Units 2&3 Calculation N-4080-005, Revision 0, "MSLB Analysis for Environmental Qualification". (dated 3/15/78) PB 1-10-94
- g. SONGS Units 2&3 Calculation N-4080-002, Revision 1, "Containment Press.-Temp Transient Analysis" (dated 10/19/76).
- h. SONGS Units 2&3 Calculation N-4080-003, Revision 5, "Containment Spray (CS) and Emergency Fan (EF) Actuation Times" (dated 12/23/93).

6.2 Correspondence

- a. Letter from CE to BPC, S-CE-2604, dated March 1, 1976. (CDM number C760301G-45-2-4SVT).
- b. Letter from CE to BPC, S-CE-4007, dated June 29, 1977. (CDM number C770629G-8-26)
- c. Letter from CE to BPC, S-CE-6814 dated August 24, 1981. (CDM number C810824G).

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6.3 Licensing Documents

- a. San Onofre Unit 2 Operating License and Technical Specifications, up to and including Amendment 101.
- b. San Onofre Unit 3 Operating License and Technical Specifications, up to and including Amendment 90.
- c. SONGS 2&3 Updated Final Safety Analysis Report (UFSAR), up to and including Revision 9.

6.4 Regulatory Documents

- a. 10 CFR Part 50, ""Domestic Licensing of Production and Utilization Facilities". Revised as of January 1, 1993.
- b. NUREG-0588, Rev 1, "Interim Staff Position on Environmental Qualification of Safety-Related Electrical Equipment".
- c. NUREG-0800, Standard Review Plan 6.2.1.1.A, Revision 2, July 1981. "PWR Dry Containments, Including Subatmospheric Containments".

6.5 Bechtel Computer Programs

a. Bechtel Standard Computer Program, MAP-175, COPATTA, Version G1-14, "Containment Pressure and Temperature Transient Analysis", User & Theory Manuals.

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6.6 Design Basis Document Reports

a. DBD-SO23-400, Revision 0, "Component Cooling Water System" (dated 12/27/91).

System Descriptions 6.7

SD-SO23-360, Revision 2, "Reactor Coolant System".

6.8 Drawings

a. P&ID 40172A, (Rev 7) Containment HVAC System (Emergency)-System No. 1501

6.9 Open Item Reports

- a. Open Item Report 92-015, Accepted 1/15/92.
- b. Open Item Report 92-045, Accepted 2/11/92.
- c. Open Item Report 92-054, Accepted 2/13/92.
- d. Open Item Report 92-057, Accepted 2/20/92
- e. Open Item Report 92-059, Accepted 2/20/92
- f. Open Item Report 92-069, Accepted 2/25/92
- Crane Technical Paper No.410, "Flow of Fluids", Twenty Fourth Printing-1988. 6.10
- Bechtel Topical Report BN-TOP-3, Revision 4, "Performance and Sizing of Dry; 6.11 Pressure Containments", dated March 1983.
- Bechtel Nuclear Design Standard N2.3.2, Revision 0, "Containment Analysis, dated July 6.12 1975.

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- 1989 ASHRAE Handbook of Fundamentals, I-P Edition, published by the American 6.13 Society of Heating, Refrigeration and Air Conditioning Engineers, Inc., Atlanta, Georgia, 1989.
- ASME Steam Tables, Fifth Edition, published by the American Society of Mechanical 6.14 Engineers".
- Shao Ti Hsu, Engineering Heat Transfer, published by D. Van Nostrand Company, Inc. 6.15 of Princeton, New Jersey, 1963.
- 6.16 NCRs 93030001, 93030002, 93030003, and 93030004. All dated 12/21/93.

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7 NOMENCLATURE

CCS	Containment	Cooling	System	(Containment	Air	Cooling	System)	
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CCWS Component Cooling Water System

Combustion Engineering CE

Containment Spray Actuation Signal CSAS

CSS Containment Spray System

Chemical and Volume Control System CVCS

DESLS Double Ended Suction Leg Slot

Engineered Safety Features Actuation Signal ESFAS

HPSI High Pressure Safety Injection HTC Heat Transfer Coefficient

Heating, Ventilation and Air Conditioning HVAC

Limiting Condition of Operation LCO

LOCA Loss of Coolant Accident LOOP Loss of Offsite Power

LPSI Low Pressure Safety Injection

MOV Motor Operated Valve NCR Non-Conformance Report NSSS Nuclear Steam Supply System RAS Recirculation Actuation Signal

RB Reactor Building

Reactor Coolant System RCS RWST Reactor Water Storage Tank

SDCHX Shutdown Cooling Heat Exchanger SIAS Safety Injection Actuation Signal

SIS Safety Injection System SIT Safety Injection Tank Ultimate Heat Sink UHS

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8.1 COPATTA CODE INPUT DATA

Section 8.1.1 presents the title card. Sections 8.1.2 through 8.1.25 will provide input data for the variable data series, while Sections 8.1.27 through 8.1.33 will provide input data for the heat sink data series. Section 8.1.26 presents the variable end card, and Section 8.1.33 presents the end card.

Item 1 in all Card Series is the Card Series Identifier, i.e. the Card Series number.

8.1.1 TITLE CARD

This card must precede each set of base case data. It must contain an asterisk in Column 1, and any combination of numeric and alphanumeric characters in the remaining 79 columns. The information on this card will appear at the top of each page of output for this prime case problem. This calculation evaluates a 7.4765 ft² MSLB at 102% power, with the containment heat removal systems affected by a single failure (i.e. only one of two cooling trains is functional) with offsite power available.

* MSLB CASE, 102% POWER, LOSS OF ONE COOLING TRAIN, OFFSITE POWER AVAIL.

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8.1.2 CARD SERIES 0: Option Information

Card Series 0 provides option information, This Card Series is entered in the input data file as:

&LIST POOL=0,0,1,0,1,0,0,0,0/

The entries in Card Series 0 include:

Item 2: IHEAT = 0

> A value of 0 indicates that no heat exchanger is modeled for containment spray per Design Input Item 4.1.a.

Item 3: NOIT = 1

> A value of 0 enables the option to iterate for the estimated time to peak pressure, and a value of 1 disables the option. Per the COPATTA User's Manual (Reference 6.5.a), iteration is not to be requested unless use of the Tagami heat transfer coefficient (HTC) is specified for the HTC control on Heat Sink Card Series 1XX400. As noted in Design Input 4.8, only the Uchida heat transfer coefficient correlation is modeled in an MSLB analysis. Therefore, no iteration for the time to peak pressure is required.

Item 4: NPTOP = 0

A value of 0 requests a normal set of data at each printout time step.

As recommended by sheet 4 of Bechtel Nuclear Standard N2.3.2 (Reference 6.12), a normal set of data should be requested at each printout time step.

Item 5: LAST = 1

A value of 1 indicates that this is the last case in a series of COPATTA Code runs.

As discussed on page 3-11 of the COPATTA User's Manual (Reference 6.5.a), the option to terminate must equal 1 because the change case option is not active.

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iten 6: IUHS TYPE = 0

A 'alue of 0 indicates that no Ultimate Heat Sink (UH' to be modeled.

Item 7: IHE SRC = 0

> A value of 0 indicates that the constant temperature and mass flow rate defined in Items 5 and 6 of Card Series 4 will be used for the Shutdown Cooling Heat Exchanger (SDCHX) data.

Item 8: IEX HE TYPE = 0

> This parameter is used to model external heat loads if the value of IHEAT is greater than or equal to four in Item 2 of Card Series 0. In this analysis IHEAT is assigned a value of 2, so any value may be modeled for IEX HE TYPE. Therefore, a value of 0 is arbitrarily chosen to be modeled.

Item 9: IHE UAMOD = 0

> A value of 0 indicates that the COPATTA Code should use the SDCHX overall heat transfer coefficient on Item 4 of Card Series 4 as a constant.

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8.1.3 CARD SERIES 1: General Problem Information

Card Series 1 provides general problem information. This Card Series is entered in the input data file as either, for the preliminary run:

&LIST POOL=1,1E4,16.2,2.305E6,120,0.6,20,582.945,1,1,0,14.7,0.50/

The entries in Card Series 1 include:

ITEM 2: TFNL = 1E4 seconds

Calculations for this analysis will be terminated at 10,000 seconds (2.78 hours). As shown in the summary of results, this analysis termination time is sufficient to ensure determination of the peak pressure and temperature time of occurrence. By this termination time the containment pressure and temperature have also returned to near initial conditions.

As discussed in Design Input Item 4.5.b, if a run time in excess of 10,000 seconds were to be modeled, then the model should also reflect actuation of the containment spray recirculation mode (spray water source transferred from the Refueling Water Storage Tank to the containment sump), and the corresponding use of the Shutdown Cooling Heat Exchanger.

ITEM 3: PAIR = 16.2 psia

The initial pressure inside the Containment prior to the start of the MSLB mass and energy release is 16.2 psia (1.5 psig), as discussed in Design Input Item 4.2.a.

ITEM 4: VOL = $2.305E6 \text{ ft}^3$

The containment net free volume is 2.305E6 ft³, as discussed in Design Input Item 4.2.b.

ITEM 5: TAIR = 120 °F

The containment atmosphere temperature prior to the start of the MSLB mass and energy release is 120 °F, as discussed in Design Input Item 4.2.c.

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ITEM 6: HUM = 0.6

The relative humidity of the atmosphere inside the Containment prior to the start of the MSLB mass and energy release is 60 percent, as discussed in Assumption 3.1.a.

ITEM 7: NSL = 20

As detailed in Section 8.1.27, twenty Heat Sinks are modeled in this calculation.

ITEM 8: TBOIL = 582.945 °F

The temperature of the primary coolant prior to the start of the MSLB mass and energy release is 582.945 °F, as discussed in Design Input 4.2.d. This value sets the initial temperature of all heat conducting region surfaces in contact with the primary coolant.

ITEM 9: TCHECK = 1 second

If the option to iterate for peak pressure is enabled (Item 3 on Card Series 0 is zero), then the variable TCHECK represents the time in seconds up to which the program will search for a second pressure peak after a first one has been located. The time to a second pressure peak is used to determine the condensation heat transfer coefficient; this quantity is used with the modified Tagami condensing heat transfer coefficient.

Per Design Item 4.8, the Uchida value will be used for the heat transfer coefficient in a MSLB. Therefore the option to iterate for peak pressure is disabled (Item 3 on Card Series 0 is one). If the TCHECK variable is not used, Bechtel Nuclear Design Standard N2.3.2 (Reference 6.12, page 5) states that the variable should be assigned a value of 1 second.

ITEM 10: THSDD = 1 second

> This variable is only used if Tagami condensation heat transfer coefficient (HTC) calculations are inodeled. As noted in Design Input 4.8, only the Uchida HTC correlation is modeled in an MSLB analysis. Therefore, any value may be entered for this variable. In this MSLB analysis the variable THSDD is modeled with an arbitrary value of 1 second.

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ITEM 11: EVAP = 0

> The fraction of heat condensate which will be allowed to revaporize is zero. No credit for revaporization is taken in this analysis per Assumption 3.1.b.

ITEM 12: ENVRNP = 14.7 psia

The total pressure outside containment is assumed to be 14.7 psia per Assumption 3.1.c.

ITEM 13: ENVRH = 0.50

> The relative humidity of the outside atmosphere is assumed to be 50 percent per Assumption 3.1.d.

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8.1.4 CARD SERIES 2: Additional General Problem Information

Card Series 2 provides additional general problem information. This Card Series is entered in the input data file as:

&LIST POOL=2,0,0,0,0,0,120,2E7/

The entries in Card Series 2 include:

ITEM 2: MWATR = 0 lbs

No water is to be introduced as a step input at the time blowdown starts.

ITEM 3: UTOT = 0 BTU

The total enthalpy associated with the water entered as variable MWATR is arbitrarily set to 0 BTU (any value is acceptable since variable MWATR is set to 0 pounds).

ITEM 4: MLEFT = 0 lbm

The variable MLEFT is the number of pounds of water left in the primary system available to be evaporated by reactor decay heat (Card Series 101) or metal water reaction heat (Card Series 201). This parameter is required for a LOCA analysis, not a MSLB analysis.

ITEM 5: REVOL = 0 ft^3

The reactor volume below the pipe rupture is 0 ft3. This parameter is required for a LOCA analysis, not a MSLB analysis.

ITEM 6: HAB = 0 BTU/hr-°F

The total heat transfer coefficient for the heat transfer between liquid (sump) and vapor regions of the containment is modeled as 0 BTU/hr-°F per Assumption 3.2.a.

ITEM 7: TCONT = 120 °F

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If the temperature boundary control on Heat Sink Card Series 1XX400 equals zero, then the variable TCONT is used to define the convective heat transfer coefficient and the bulk temperature to which the heat sink surfaces are exposed. Each of the twenty heat sinks modeled in this analysis assigns the temperature boundary control on Heat Sink Card Series 1XX400 a value other than zero. Since the variable TCONT is not used, Bechtel Nuclear Standard N2.3.2 (Reference 6.12, page 5) states that any positive value may be modeled. Since the COPATTA Code input files of Calculation N-4080-007 (Reference 6.1j) employed an arbitrary value of 120 °F, this analysis will also model an arbitrary value of 120 °F.

ITEM 8: PHELP = 2E7 seconds

The time at which mass and energy balance calculations for the water within the reactor vessel will begin is 2E7 seconds. This parameter is required for a LOCA analysis, not a MSLB analysis, therefore any time greater than the analysis run time may be used.

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8.1.5 CARD SERIES 3: Leakage from Containment

Card Series 3 allows modeling of the addition and/or deletion of air/steam via containment HVAC operation. No credit is taken for HVAC operation in this MSLB analysis: Therefore, this Card Series is entered in the input data file as:

&LIST POOL=3,0,0,0,0,0,2E7,0,0,0,0/

The entries in Card Series 3 include:

ITEM 2: 0 seconds

The HVAC start time is 0 seconds.

ITEM 3: 0 ft3/minute

The initial HVAC volume addition rate is 0 ft³/minute.

ITEM 4: 0 °F

The initial temperature of the air added is 0 °F.

ITEM 5: 0 percent

The initial relative humidity of the air added is 0 percent.

ITEM 6: 0 ft3/minute

The initial HVAC volume removal rate is 0 ft³/minute.

ITEM 7: 2E7 seconds

The HVAC stop time is 2E7 seconds. 'This time must be longer than the analysis run time.

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ITEM 8: 0 ft3/minute

The final HVAC volume addition rate is 0 ft³/minute.

ITEM 9: 0 °F

The final temperature of the air added is 0 °F.

0 percent ITEM 10:

The final relative humidity of the air added is 0 percent.

ITEM 11: 0 ft³/minute

The final HVAC volume removal rate is 0 ft³/minute.

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8.1.6 CARD SERIES 4: Heat Exchanger Data

Card Series 4 provides for simulation of heat exchangers for long term analysis of the effectiveness of the containment spray and safety injection systems.

Card Series 4 also provides for a means of starting the containment spray. The COPATTA Code compares two potential starting times for the containment spray, and starts the air coolers at the later of the two times. The first time is specified by the first non-zero spray flow entry in Card Series 801, Item 2. The second time, TNOW, is defined as the sum of the time at which the spray initiation signal (Item 12) is reached, and the instrumentation and equipment delay time (Item 13). In this analysis, the desired containment spray start time is to be the time modeled in Card Series 801. To ensure that the Card Series 801 time is used by the COPATTA Code, the Items 12 and 13 variables are modeled as 0 psia and 0 seconds, respectively. This leads to the calculation of a containment spray start time of 0 seconds for the variable TNOW, and forces the code to employ the larger time specified in Card Series 801.

This Card Series is entered in the input data file as:

&LIST POOL=4,0,0,0,0,0,0,0,0,0,0,0,0,0/

The entries in Card Series 4 include:

ITEM 2: IHEX = 0

A value of 0 indicates that a primary heat exchanger will not be modeled in this analysis. As discussed in Design Input Item 4.1.a, the Shutdown Cooling Heat Exchanger (SDCHX) will not be modeled in this MSLB analysis.

ITEM 3: HEX (1) = 0 ft^2

The primary heat exchanger surface area. Since no primary heat exchanger is modeled, a value of zero is used for this variable.

ITEM 4: HEX (2) = 0 BTU/hr-ft^2 -°F

The overall heat exchanger heat transfer coefficient. Since no primary heat exchanger is modeled, a value of zero is used for this variable.

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ITEM 5: HEX (3) = 0 °F

The primary heat exchanger coolant inlet temperature. Since no primary heat exchanger is modeled, a value of zero is used for this variable.

ITEM 6: HEX (4) = 0 lbm/hr

The primary heat exchanger coolant flow rate. Since no primary heat exchanger is modeled, a value of zero is used for this variable.

ITEM 7: IHIX = 0

A value of 0 indicates that no secondary heat exchanger is modeled in this analysis.

ITEMS 8 through 11: 0, 0, 0, 0

These entries are all zero, since there are no secondary heat exchangers in use.

Per the COPATTA Code Users Manual (Reference 6.5.a, page 3-20), if only a primary heat exchanger is used, zeroes should be input for Items 7 through 11, and 14.

ITEM 12: 0 psia

> As discussed in the introduction to this Card Series 4, the containment spray pressure initiation signal is modeled as 0 psia.

ITEM 13: 0 seconds

> As discussed in the introduction to this Card Series 4, the instrumentation and equipment delay time after receiving the pressure signal is modeled as 0 seconds.

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ITEM 14: DMINL = 0 lb/hr

This entry is zero, since there are no secondary heat exchangers in use.

Per the COPATTA Code Users Manual (Reference 6.5.a, page 3-20), if only a primary heat exchanger is used, zeroes should be input for Items 7 through 11, and 14.

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8.1.7 CARD SERIES 5: Air Cooler Information

Card Series 5 provides for the selection of the number of containment air coolers operating, and the period of operation. The air cooler heat removal capability curve is read into the problem in Card Series 1101.

The COPATTA Code compares two potential starting times for the air coolers, and starts the air coolers at the later of the two times. The first time is specified by Item 3. The second time, TNOW, is defined as the sum of the time at which the air cooler initiation signal (Item 5) is reached, and the TDELAY signal processing delay time (Item 6). In this analysis, the desired air cooler start time is to be the time modeled in Item 3. To ensure that the Item 3 time is used by the COPATTA Code, Items 5 and 6 variables are modeled as 0 psia and 0 seconds, respectively. This leads to the calculation of an air cooler start time of 0 seconds for the variable TNOW, and forces the code to employ the larger time specified in Item 3.

Card Series 5 is entered in the input data file as:

&LIST POOL=5,2,15,1E4,0,0,0,105/

The entries in Card Series 5 include:

ITEM 2: 2

There are two containment air coolers modeled in this analysis as discussed in Assumption 3.3.a.

ITEM 3: 15 seconds for MSLB with offsite power available.

The value represents the air coolers' starting time of 15 seconds as discussed in Design Input Item 4.3.a.

ITEM 4: 1E4 seconds

The shutoff time for the air coolers is modeled as 1E4 seconds. Use of this time will ensure that the containment air coolers will operate for the duration of the accident, as discussed in Assumption 3.3.b.

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ITEM 5: 0 psia

As discussed in the introduction to this Card Series 5, the air cooler pressure initiation signal is modeled as 0 psia.

ITEM 6: TDELAY = 0 seconds

As discussed in the introduction to this Card Series 5, the instrumentation delay time after receiving the pressure signal is modeled as 0 seconds.

ITEM 7: IAC SRC = 0

A value of 0 indicates that the air cooler heat exchanger coolant temperature is the constant value given in Item 8 of this Card Series 5.

ITEM 8: 105 °F

The temperature of the air cooler heat exchanger coolant is 105 °F as discussed in Design Input Item 4.3.b.

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8.1.8 CARD SERIES 6: Instantaneous Release of Energy

Card Series 6 provides for the instantaneous release of a specified amount of energy (to the containment atmosphere, containment sump, or to the reactor vessel water) at any one time during the accident. However, other than blowdown, no instantaneous release of energy is modeled in this analysis. Therefore, Card Series 6 is entered in the input data file as:

&LIST POOL=6, 0, 0, 0/

ITEM 2: TPULSE = 0 seconds

Per the COPATTA Code Users Manual (Reference 6.5.a, page 3-23), zeroes may be input for Items 2 through 4 if an instantaneous release of energy is not modeled.

ITEM 3: IPULSE = 0

Per the COPATTA Code Users Manual (Reference 6.5.a, page 3-23), zeroes may be input for Items 2 through 4 if an instantaneous release of energy is not modeled.

ITEM 4: UPULSE = 0 BTU

Per the COPATTA Code Users Manual (Reference 6.5.a, page 3-23), zeroes may be input for Items 2 through 4 if an instantaneous release of energy is not modeled.

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8.1.9 CARD SERIES LEAK: Leakage Paths Between Containment and Outside Atmosphere.

No leakage from containment to outside containment is modeled in this analysis. This Card Series is entered in the input data file as:

&LEAK NOPEN=0/

The variable NOPEN is equal to zero because the number of openings in the containment is zero.

Per the COPATTA Code Users Manual (Reference 6.5.a, page 3-25), if NOPEN is equal to zero, then the other variables may be omitted from the Card Series LEAK.

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8.1.10 CARD SERIES 101: Reactor Core Decay Power (Table 2)

Card Series 101 is a table that is used to input reactor core decay power. This table is used in combination with information provided in Card Series 401 and 701. The reactor core decay power table includes up to 25 sets of the following data entered in columnar form:

- 1. Time (seconds)
- 2. Decay Power Generation rate (BTU/hr)

Reactor core decay heat is not modeled in the COPATTA input for this MSLB analysis. Any core decay heat impacting the containment P/T response to the event has already been included by CE in their calculation of the mass and energy release data which are separately input in Card Series 301 data. Therefore, Card Series 101 shall be entered as:

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8.1.11 CARD SERIES 201: Reactor Metal-Water Reaction (Table 3)

Card Series 201 is a table that is used to input reactor metal-water reaction rate. This table is used in combination with information presented in Card Series 401 and 701. The combined reactor metal-water reaction includes up to 25 sets of the following data, entered in columnar form:

- 1. time (seconds)
- 2. energy release rate (Btu/hour)

Since reactor metal-water reaction is not modeled in an MSLB analysis, Card Series 201 shall be entered as:

&LIST POOL=201, 0, 0/ 2E7,

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8.1.12 CARD SERIES 301: Blowdown Following Pipe Rupture (Table 4)

Card Series 301 is a table that is used to input blowdown following the pipe rupture. The blowdown table includes up to 200 sets of the following data entered in columnar form:

- 1. time (seconds)
- 2. water addition rate (pounds/hour)
- 3. enthalpy of the water being added (BTU/pound)

The input data to be used in Card Series 301 is discussed in Design Input Item 4.4. This Card Series is entered in the input data file as shown below. The mass and energy release rates are assumed to vary linearly between each data point.

```
&LIST POOL=301,
    0, 5.145520E7, 1.195589E3,
 0.22,
         4.869032E7, 1.197482E3,
 0.42,
         4.622234E7, 1.198466E3,
 0.62,
         4.405936E7, 1.199410E3,
 1.08,
         4.003276E7, 1.201595E3,
 1.58,
        3.688855E7, 1.201757E3,
 2.08,
        3.445970E7, 1.202018E3,
 2.58,
         3.326288E7, 1.200986E3,
         3.152606E7, 1.201058E3, 3.028468E7, 1.201655E3, 2.940080E7, 1.201123E3,
 3.58,
 4.58,
 5.58,
 6.58,
         2.874870E7, 1.201126E3,
 7.58,
         2.706574E7, 1.204404E3,
 8.58,
         2.468326E7, 1.204367E3,
 9.58,
        2.294968E7, 1.204238E3,
10.58,
        2.160122E7, 1.203908E3,
12.58,
        1.943143E7, 1.203195E2,
        1.765940E7, 1.202277E3,
1.637240E7, 1.201556E3,
1.544720E7, 1.200963E3,
1.473293E7, 1.200422E3,
14.58,
16.58,
18.58,
20.58,
25.58,
         1.327525E7, 1.198820E3,
30.58,
         1.221858E7, 1.197825E3,
35.58,
         1.146406E7, 1.196753E3,
40.58,
         1.059131E7, 1.195307E3,
        9.801216E6, 1.194165E3,
9.132588E6, 1.193086E3,
8.280324E6, 1.190935E3,
45.58,
50.58,
60.58,
         7.245576E6, 1.190949E3,
61.08,
62.08,
        5.803344E6, 1.189165E3,
62.58,
        3.238704E6, 1.184658E3,
64.58,
        3.948840E5, 1.179953E3,
68.58, 1.074240E5, 1.251072E3,
                    0,
71.08,
                                   0,
                    0,
  2E7,
                                   0/
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8.1.13 CARD SERIES 401: (Table 5)

Card Series 401 is a table that is used to describe the energy addition to the reactor vessel water from core decay power (Card Series 101) and any metal-water reaction (Card Series 201). This table designates the fraction of each of these energy sources that is added to the energy inventory in the reactor vessel. This table includes up to 20 sets of the following data entered in columnar form:

- 1. time (seconds)
- 2. decay power multiplier (dimensionless)
- 3. metal-water reaction multiplier (dimensionless)

Since reactor core decay energy and reactor metal-water reaction energy are not modeled in an MSLB analysis, Card Series 401 shall be entered as:

&LIST POOL=401, 0, 0, 0, 2E7, 0, 0/ 2E7,

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CARD SERIES 501: Blowdown Following Pipe Rupture (Table 4) 8.1.14

This Card Series is used only if number of points are more than can fit in Card Series 301. The Card Series 501 table includes up to 200 sets of the following data entered in columnar form:

- 1. time (seconds)
- 2. water addition rate (pounds/hour)
- 3. energy addition rate (BTU/hour)

Card Series 501 is not needed since Card Series 301 had enough space for all data. Therefore, Card Series 501 shall be entered as:

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8.1.15 CARD SERIES 601: (Table 7)

This Card Series is used to add water and/or energy directly to the containment sump, regardless of the enthalpy of the water being added. This card is generally used to describe the spillage of Emergency Core Cooling System (ECCS) injection water that overflows the reactor vessel downcomer when the vessel is full. The Card Series 601 table includes up to 80 sets of the following data entered in columnar form:

- 1. time (seconds)
- 2. water addition rate (pounds/hour)
- 3. energy addition rate (BTU/hour)

Since additional water or energy are not added directly to the containment sump in an MSLB analysis, Card Series 601 shall be entered as:

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8.1.16 CARD SERIES 701: (Table 8)

Card Series 701 is a table that is used to describe the energy addition to the containment atmosphere from core decay power (Card Series 101), the metal-water reaction (Card Series 201). This table designates the fraction of each of these energy sources that is added to the energy inventory in the containment atmosphere. Card Series 701 also provides for arbitrary addition of water mass to the containment atmosphere. This table includes up to 20 sets of the following data entered in columnar form:

- 1. time (seconds)
- 2. decay power multiplier (dimensionless)
- 3. metal-water reaction multiplier (dimensionless)
- 4. water addition rate (pounds/hour)

Since reactor core decay energy or reactor metal-water reaction energy are not modeled in an MSLB analysis and no arbitrary addition of water mass was added to the containment atmosphere, Card Series 701 shall be entered as:

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8.1.17 CARD SERIES 801: (Table 9)

Card Series 801 is a table that provides input of information on the characteristics of the containment spray system, the core safety injection system, and the source of water supply for these systems. The Card Series 801 table includes up to 16 sets of the following data entered in columnar form:

- 1. time (seconds)
- 2. containment spray flow rate (pounds/hour)
- 3. reactor core safety injection water flow rate (pounds/hour)
- 4. fraction of the safety injection flow poured directly into the containment sump due to injection into a ruptured pipe (dimensionless)
- 5. water temperature of containment spray (°F)
- 6. water temperature of safety injection (°F)

This Card Series is discussed in Design Input Item 4.5. Card Series 801 shall be entered in the input data file as:

&LIST	POOL	=801,				
	0,	0,	0,	0,	100,	100,
	50,	0,	0,	0,	100,	100,
	50,	8.02E5,	0,	0,	100,	100,
-	2E7,	8.02E5,	0,	0,	100,	100/

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CARD SERIES 901: (Table 10) 8.1.18

Card Series 901 provides for the arbitrary addition of air to the containment atmosphere. The arbitrary air addition table includes up to 20 sets of the following data entered in columnar form:

- 1. time (seconds)
- 2. containment air addition rate (pounds/hour)
- 3. temperature of the added air (°F)

Since no arbitrary air addition is modeled in this analysis, Card Series 901 shall be entered as:

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8.1.19 CARD SERIES 1001: (Table 11)

Card Series 1001 is used to determine the effect of cyclic outside temperature variations on long term post-accident temperature and pressure transients within the containment. The time period covered by the data should be from zero to 24 hours. The program will then use the data for succeeding 24 hour periods in very long time problems. The cyclic outside temperature variation table includes up to 25 sets of data entered in columnar form:

- 1. time (seconds)
- 2. temperature of the outside air (°F)
- 3. heat transfer coefficient between a heat sink and the outside atmosphere (BTU/hr-ft2-°F)

In this MSLB model, no time-dependent atmospheric variations are modeled, and therefore the same data values are entered at times 0 and 24 hours. Card Series 1001 is entered in the put data file as:

&LIST POOL=1001. 0, 100, 2.0, 24, 100, 2.0/

The entries in Card Series 1001 include:

ITEM 2: 0 hours

The initial time in hours. The starting time of the first 24 hour cycle is 0 hours.

ITEM 3: 100 °F

The outside air temperature at the start of the first 24 hour cycle is assumed to be 100 °F as discussed in Assumption 3.4.a.

ITEM 4: 2.0 BTU/hr-ft²-°F

The heat transfer coefficient between a heat sink and the outside atmosphere at the start of the first 24 hour cycle is assumed to be 2.0 BTU/hr-ft2-°F as discussed in Assumption 3.4.b.

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ITEM 5: 24 hours

The ending time of the first 24 hour cycle is 24 hours.

ITEM 6: 100 °F

The outside air temperature at the end of the first 24 hour cycle is assumed to be 100°F as discussed in Assumption 3.4.a (same as at the start of the cycle).

ITEM 7: 2.0 BTU/hr-ft2-°F

The heat transfer coefficient between a heat sink and the outside atmosphere at the end of the first 24 hour cycle is assumed to be 2.0 BTU/hr-ft2-°F as discussed in Assumption 3.4.b (same as at the start of the cycle).

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8.1.20 CARD SERIES 1101: (Table 12)

As defined by Item 2 of Card Series 5, two containment air coolers are modeled in this analysis. Card Series 1101 is used to describe the heat removal capability of one air cooler as a function of containment atmosphere saturation temperature. Card Series 1101 provides for a table of tables, each table representing a discrete air cooler coolant temperature.

Card Series 1101 is entered in the DBA MSLB input data file as:

```
&LIST POOL=1101, 1, 21, 105,
           105,
           120, 1.670E6,
130, 3.020E6,
140, 4.570E6,
            150, 6.320E6,
            160, 8.270E6,
            170,
                  1.040E7
            180,
                  1.273E7,
            190,
                  1.523E7
            200,
                  1.788E7.
            210,
                  2.068E7,
            220,
                  2.361E7,
            230,
                  2.661E7.
            240,
                  2.974E7,
            250,
                  3.291E7
            260, 3.611E7,
            270, 3.931E7,
                 4.252E7,
            280,
           287, 4.474E7,
           290, 4.569E7
           300, 4.882E7/
```

The entries in Card Series 1101 include:

ITEM 2: INUM=1

The value of 1 indicates that only one table of air cooler heat removal capability as a function of containment atmosphere saturation temperature is modeled. Separate tables are required for each air cooler coolant temperature, and this analysis only models a single air cooler coolant temperature.

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ITEM 3: 21

A value of 21 indicates that there are twenty-one sets of data in the table (Items 5 and 6) describing air cooler heat removal capability as a function of containment atmosphere saturation temperature.

ITEM 4: 105 °F

The table (Items 5 and 6) describing air cooler heat removal capability as a function of containment atmosphere saturation temperature is based on an air cooler inlet temperature of 105 °F, as discussed in Design Input 4.3.b.

ITEMS 5 and 6

Containment atmosphere saturation temperature (°F), and Corresponding cooler heat removal rate (BTU/hour)

The input data to be used in defining the Items 5 and 6 entries are discussed in Design Input Item 4.6.a.

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8.1.21 CARD SERIES 1105: UHS Parameters

Card Series 1105 is used to provide the Ultimate Heat Sink (UHS) parameters as a function of time. Since no UHS are modeled in this analysis (See Item 6 of Card Series 0), Card Series 1105 is not included in the input file.

8.1.22 CARD SERIES 1106: External Heat Load/Sink

Card Series 1106 is used to describe the time behavior of an external heat load/sink that is used only when IHEAT Option 5, 6 and 7 is defined for Item 2 of Card Series 0. In this analysis, Item 2 of Card Series 0 is defined as 2, therefore Card Series 1106 is not included in the input file.

8.1.23 CARD SERIES 1110: Heat Transfer Coefficient Multipliers

Card Series 1110 describes the time behavior of the overall heat transfer coefficients for the primary and secondary heat exchangers used in the system. These values are multipliers for the values on Items 4 and 9 of Card Series 4, for the primary and secondary heat exchangers, respectively. In this analysis, no heat exchangers are modeled. The overall SDCHX heat transfer coefficient defined in Item 4 of Card Series 4 is a constant value, therefore Card Series 1110 is not included in the input file.

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8.1.24 CARD SERIES 1201: Table 13

Card Series 1201 provides for variation in the containment spray efficiency as a function of the ratio of water vapor to air mass in the containment atmosphere. The containment spray efficiency table includes up to 40 sets of the following data entered in columnar form:

- 1. (RATIO) the containment steam/air mass ratio (dimensionless)
- 2. (ETANOZ) spray efficiency (fraction)

This Card Series is discussed in Design Input Item 4.7.a. Card Series 1201 is entered in the input data file as:

&LIST POOL=1201, 0, 0.729, 0.1, 0.737, 0.2, 0.747, 0.3, 0.757, 0.771, 0.4, 0.5, 0.788, 0.6, 0.809, 0.7, 0.832, 0.8, 0.863, 0.9, 0.912, 1.0, 0.561, 1.1, 0.983, 1.2, 0.995, 1.3, 1.000/

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8.1.25 CARD SERIES 9001: Table 14

Card Series 9001 is used to specify the calculational time intervals and the data printout intervals. The calc/print time table includes up to 50 sets of the following data entered in columnar form:

- 1. time (seconds)
- 2. calculational interval (seconds)
- 3. energy balance printout interval (seconds)
- 4. heat sink printout frequency (dimensionless)

Card Series 9001 is entered in the input data file as:

```
&LIST POOL=9001,
             5,
                0.05,
                         0.1,
                                50,
             10, 0.05,
                        0.25,
                                20,
            15, 0.05,
                        0.50,
                               10,
             20, 0.05,
                        0.50,
                               10,
            100, 0.1,
                        1.0,
            200,
                 1.0,
                         5.0,
                               10,
                 1.0,
                        10.0,
            400,
                        10.0,
            700,
                                5,
                 5.0,
            2E3,
                        50.0,
            1E4, 50.0,
                         500,
            1E5,
                 250,
                         1E4,
                                4,
                  500,
                         1E5,
            1E6,
            1E7,
                  500,
                         5E5,
            2E7,
                  500,
                          5E5,
                                9/
```

The selection of the time steps is based on the guidance given in Bechtel Nuclear Standard N2.3.2 (Reference 6.12, sheet 14 of 24). This analysis uses a higher calculational frequency to get more accurate output data.

As shown in the following tables, for an analysis run time of 10,000 seconds (Card Series 1, Item 2), this data will generate 2070 internal calculation intervals, 267 energy balance printouts and 38 heat sink printouts.

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INTERNAL CALCULATIONAL FREQUENCY

TIME INTERVAL	TIME INTERVAL DURATION	INTERNAL CALCULATION	NUMBER OF INTERNAL
(seconds)	(seconds)	INTERVAL (every # seconds)	CALCULATIONS
0 to 5	5	0.05	100
5 to 10	5	0.05	100
10 to 15	5	0.05	100
15 to 20	5	0.05	100
20 to 100	80	0.1	800
100 to 200	100	1.0	100
200 to 400	200	1.0	200
400 to 700	300	2.0	150
700 to 2E3	1,300	5.0	260
2E3 to 1E4	8,000	50.0	160
		otal Number of Calculations:	2070

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ENERGY BALANCE PRINTOUT FREQUENCY

TIME INTERVAL (seconds)	TIME INTERVAL DURATION (seconds)	ENERGY BALANCE PRINTOUT INTERVAL (every # seconds)	NUMBER OF ENERGY BALANCE PRINTOUTS
0 to 5	5	0.10	50
5 to 10	5	0.25	20
10 to 15	5	0.50	10
15 to 20	5	0.50	10
20 to 100	80	1	80
100 to 200	100	5	20
200 to 400	200	10	20
400 to 700	300	20	15
700 to 2E3	1,300	50	26
2E3 to 1E4	8,000	500	16
	Total Number	r of Energy Balance Printouts:	267

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HEAT SINK PRINTOUT FREQUENCY

TIME INTERVAL	NUMBER OF	HEAT SINK	NUMBER OF
(seconds)	ENERGY BALANCE PRINTOUTS	PRINTOUT INTERVAL (one for every # energy printouts)	HEAT SINK PRINTOUTS
0 to 5	50	50	1
5 to 10	20	20	1
10 to 15	10	10	1
15 to 20	10	10	1
20 to 100	80	10	8
100 to 200	20	10	2
200 to 400	20	5	4
400 to 700	15	5	3
700 to 2E3	26	2	13
2E3 to 1E4	16	4	4
	Total N	umber of Heat Sink Printouts:	38

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8.1.26 VARIABLE END CARD

This card must follow the group of variable data cards. It contains the following fixed information in Columns 2 through 17:

&LIST POOL=9999/

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8.1.27 HEAT SINK DATA SERIES

The heat sink data series are used to describe the characteristics of the structural heat sinks. In this analysis twenty heat sinks are modeled (Card Series 1, Item 7). Each heat sink (number XX) is detailed in the COPATTA Code as a set of heat sink data cards. These data cards include:

Title Card

Card Series 1XX001

Card Series 1XX101

Card Series 1XX201

Card Series 1XX300

Card Series 1XX400

Card Series 1XX001 contains general information on the heat sink. Card Series 1XX101 provides information on heat sink mesh point spacing. Card Series 1XX201 specifies the set of material properties for each region of the heat sink. Card Series 1XX300 selects the type and variation in magnitude of the decay power source within the heat sink. Card Series 1XX400 is used to select the appropriate boundary conditions for the left and right surfaces of each heat sink.

In general, the presence (or increase in size) of a heat sink has two consequences: (1) depressing the peak containment pressure and temperature by absorbing energy released via the break, and (2) extending the duration of above ambient containment pressures and temperatures by releasing energy back into the containment during the latter part of the accident. Beyond these two general consequences, the impact of a change in the modeling of a heat sink (e.g., a change in the heat sink layer thicknesses) is difficult to qualify.

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8.1.27.1 HS #1 - Reactor Building Dome

The characteristics of the Reactor Building Dome are as determined in Calculation N-4080-002 (Reference 6.1.g, pages 121 through 125) for Heat Sink 1, except for the thickness of the Containment Liner/Concrete air gap interface.

As discussed in Design Input Item 4.8.a, the effective thickness of the interface (air gap) will be 0.00035 feet. With this change, Heat Sink #1 describes the Reactor Building Dome as modeled:

Geometry Slab

Surface Area 34693.22 ft2

Organic Paint (material 4) thickness-Left 0.00075 ft (= 0.009 in)

Boundary

Carbon Steel (material 1) Liner thickness 0.02083 ft (= 0.25 in)

Air Gap Interface (material 5) thickness 0.00035 ft

Concrete (material 2) thickness-Right Boundary 4.0417 ft (= 48.5 in)

Left Boundary condition Exposed to containment atmosphere

Right Boundary condition Exposed to outside environment

The effect of the change in the air gap thickness is reflected in Card Series 101101. This Card Series defines the location of the right boundary and nodalization of each region. The air gap is the third region of Heat Sink 1. The increase in the modeled air gap thickness from 0.00017 feet to 0.00035 feet requires that the modeled location of the Region 3 right boundary be increased by 0.00018 feet. To maintain the correct thickness of each Region that follows the air gap region necessitates that the modeled locations of the right boundaries of these subsequent regions be increased by the same 0.00018 feet. The changes from the right boundary locations determined in Calculation N-4080-002 are:

1st Region: no change in the right boundary location 2nd Region: no change in the right boundary location

3rd Region: right boundary shifted from 0.02175 to 0.02193 feet 4th Region: right boundary shifted from 0.06342 to 0.06360 feet 5th Region: right boundary shifted from 0.2301 to 0.23028 feet 6th Region: right boundary shifted from 1.000921 to 1.00110 feet 7th Region: right boundary shifted from 4.06345 to 4.06363 feet

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The Card Series set defining Heat Sink 1 is entered in the input data file as:

```
* HS #1 - REACTOR BUILDING DOME
 &LIST POOL=101001, 100, 7, 0, 0, 0, 0, 34593.22/
&LIST POOL=101101, 5, 0.00075, 3, 0.02158, 3, 0.02193, 10, 0.06360,
                      20, 0.23028, 37, 1.00110,
                      21, 4.06363/
 &LIST POOL=101201, 4, 1, 5, 2, 2, 2, 2/
 &LIST POOL=101300, 0, 0/
&LIST POOL=101400, 9, 2, 1, 1/
```

As discussed in Design Input 4.8, the heat transfer coefficient control for the left boundary condition (adjacent to the organic paint) is modeled as the Uchida value. This is a condensing steam value dependent on the ratio of water vapor to air used in MSLB analyses. Therefore Item 2 in Card Series 101400 is 9.

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8.1.27.2 HS #2 - Reactor Building Cylinder #1 (above grade, between El. 29'6" and 112'0")

The characteristics of the Reactor Building Cylinder #1 (above grade, between plant elevations 29'6" and 112'0") are as determined in Calculation N-4080-002 (Reference 6.1.g, pages 125 through 128) for Heat Sink 2, except for the thickness of the Containment Liner/Concrete air gap interface.

As discussed in Design Input Item 4.8.a, the effective thickness of the interface (air gap) will be 0.00035 feet. With this change, Heat Sink #2 describes the Reactor Building Cylinder 1 as modeled:

Geometry Slab

Surface Area 38120 ft²

Organic Paint (material 4) thickness-Left 0.00075 ft (= 0.009 in)

Boundary

Carbon Steel (material 1) Liner thickness 0.02083 ft (= 0.25 in)

Air Gap Interface (material 5) thickness 0.00035 ft

Concrete (material 2) thickness-Right Boundary 4.33333 ft (= 52 in)

Left Boundary condition Exposed to containment atmosphere Right Boundary condition Exposed to outside environment

The effect of the change in the air gap thickness is reflected in Card Series 102101. This Card Series defines the location of the right boundary and nodalization of each region. The air gap is the third region of Heat Sink 2. The increase in the modeled air gap thickness from 0.00017 feet to 0.00035 feet requires that the modeled location of the Region 3 right boundary be increased by 0.00018 feet. To maintain the correct thickness of each Region that follows the air gap region necessitates that the modeled locations of the right boundaries of these subsequent regions be increased by the same 0.00018 feet. The changes from the right boundary locations determined in Calculation N-4080-002 are:

1st Region: no change in the right boundary location 2nd Region: no change in the right boundary location

3rd Region: right boundary shifted from 0.02175 to 0.02193 feet 4th Region: right boundary shifted from 0.06342 to 0.06360 feet 5th Region: right boundary shifted from 0.14676 to 0.14694 feet 6th Region: right boundary shifted from 0.917581 to 0.917761 feet

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right boundary shifted from 4.35508 to 4.35526 feet

The Card Series set defining Heat Sink 2 is entered in the input data file as:

```
* HS #2 - CYLINDER WALL BETWEEN E1. 29'6" AND 112'0"
&LIST POOL=102400, 9, 2, 1, 1/
```

As discussed in Design Input 4.8, the heat transfer coefficient control for the left boundary condition (adjacent to the organic paint) is modeled as the Uchida value. This is a condensing steam value dependent on the ratio of water vapor to air used in MSLP analyses. Therefore Item 2 in Card Series 102400 is 9.

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8.1.27.3 HS #3 - Reactor Building Cylinder #2 (below grade, between El. 15'0" and 29'6")

The characteristics of the Reactor Building Cylinder #2 (below grade, between plant elevations 15'0" and 29'6") are as determined in Calculation N-4080-002 (Reference 6.1.g, pages 134 through 136) for Heat Sink 3, except for the thickness of the Containment Liner/Concrete air gap interface.

As discussed in Design Input Item 4.8.a, the effective thickness of the interface (air gap) will be 0.00035 feet. With this change, Heat Sink #3 describes the Reactor Building Cylinder 2 as modeled:

Geometry Slab Surface Area 6667.38 ft² Organic Paint (material 4) thickness-Left 0.00075 ft (= 0.009 in)Boundary Carbon Steel (material 1) Liner thickness 0.02083 ft (= 0.25 in)Air Gap Interface (material 5) thickness 0.00035 ft Concrete (material 2) thickness-Right Boundary 4.33333 ft (= 52 in) Left Boundary condition Exposed to containment atmosphere Right Boundary condition Insulated, no heat transfer to the ground outside the lower portion of

Because there is no heat transfer across the right boundary, the bulk temperature control for the right boundary condition is not used by the COPATTA Code. Therefore, in this analysis the bulk temperature control for the right boundary condition is modeled as the containment vapor temperature for convective heat transfer or the saturation temperature at the containment steam partial pressure for condensing heat transfer (i.e., Option 2 for Item 5 of Card Series 1XX400). This differs from the modeling of Calculation N-4080-002, which employed Option 0 for Item 5 of Card Series 1XX400. Since the bulk temperature control for the right boundary condition has no meaning for this Heat Sink, the decision to model Item 5 with Option 2 rather than Option 0 has the beneficial consequence of allowing the use of any positive value to be modeled as the variable TCONT in Item 7 of Card Series 2.

The effect of the change in the air gap thickness is reflected in Card Series 103101. This Card Series defines the location of the right boundary and nodalization of each region. The air gap is the third region of Heat Sink 3. The increase in the modeled air gap thickness

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from 0.00017 feet to 0.00035 feet requires that the modeled location of the Region 3 right boundary be increased by 0.00018 feet. To maintain the correct thickness of each Region that follows the air gap region necessitates that the modeled locations of the right boundaries of these subsequent regions be increased by the same 0.00018 feet. The changes from the right boundary locations determined in Calculation N-4080-002 are:

1st Region: no change in the right boundary location no change in the right boundary location

3rd Region: right boundary shifted from 0.02175 to 0.02193 feet
4th Region: right boundary shifted from 0.06342 to 0.06360 feet
5th Region: right boundary shifted from 0.14676 to 0.14694 feet
6th Region: right boundary shifted from 0.917581 to 0.917761 feet
7th Region: right boundary shifted from 4.35508 to 4.35526 feet

The Card Series set defining Heat Sink 3 is entered in the input data file as:

As discussed in Design Input 4.8, the heat transfer coefficient control for the left boundary condition (adjacent to the organic paint) is modeled as the Uchida value. This is a condensing steam value dependent on the ratio of water vapor to air used in MSLB analyses. Therefore Item 2 in Card Series 103400 is 9.

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8.1.27.4 HS #4 - Basemat (other than the Reactor Basemat)

The characteristics of the Basemat (other than the Reactor Basemat) are as determined in Calculation N-4080-002 (Reference 6.1.g, pages 137 through 139) for Heat Sink 4.

Heat Sink #4 describes the Basemat (other than Reactor Basemat) as modeled:

Slab
12800 ft ²
0.00067 ft (= 0.008 in)
1.52631 ft
0.02083 ft (= 0.25 in)
9.473685 ft
Exposed to containment sump water
Insulated, no heat transfer to the ground beneath the basemat

Due to an addition error, Calculation N-4080-002 (page 138) incorrectly modeled the right boundary coordinate of the second Concrete Region at 11.02105 feet. The determination of the right boundary coordinate of the second Concrete region was based on the right boundary coordinate of the Carbon Steel Region of 1.54736 feet, rather than the correct coordinate of 1.54781 feet. In this analysis the right boundary coordinate of the second concrete region will be modeled at the correct position of 11.02150 feet:

Right Boundary Coordinate of Concrete Region #2 = 1.54781 ft + 9.473685 ft= 11.02150 feet

Because there is no heat transfer across the right boundary, the bulk temperature control for the right boundary condition is not used by the COPATTA Code. Therefore, in this analysis the bulk temperature control for the right boundary condition is modeled as the containment liquid temperature (i.e., Option 3 for Item 5 of Card Series 1XX400). This differs from the modeling of Calculation N-4080-002, which employed Option 0 for Item 5 of Card Series 1XX400. Since the bulk temperature control for the right boundary condition has no meaning for this Heat Sink, the decision to model Item 5 with Option 3 rather than Option 0

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has the beneficial consequence of allowing the use of any positive value to be modeled as the variable TCONT in Item 7 of Card Series 2.

The Card Series set defining Heat Sink 4 is entered in the input data file as:

```
* HS #4 - BASEMAT (OTHER THAN REACTOR BASEMAT)
 &LIST POOL=104001, 53, 5, 0, 0, 0, 0, 12800/
&LIST POOL=104101, 3, 0.00067, 7, 0.1,
20, 1.52698, 2, 1.54781,
                            20, 11.02150/
 &LIST POOL=104201, 4, 2, 2, 1, 2/
 &LIST POOL=104300, 0, 0/
&LIST POOL=104400, 3, 3, 0, 3/
```

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8.1.27.5 HS #5 - Reactor Basemat and Steam Generator Pedestals

The characteristics of the Reactor Basemat and Steam Generator Pedestals are as determined in Calculation N-4080-002 (Reference 6.1.g, pages 139 through 141) for Heat Sink 5.

Heat Sink #5 describes the Reactor Basemat and Steam Generator Pedestals as modeled:

Geometry Slab

Surface Area 1644 ft²

Organic Paint (material 4) thickness-Left 0.00158 ft

Boundary

Concrete (material 2) thickness-Right Boundary 8.42934 ft

Left Boundary condition Exposed to containment sump

water

Right Boundary condition Insulated, no heat transfer to the

ground beneath the basemat

In Calculation N-4080-002 (page 141) the heat transfer coefficient control for the left boundary condition was modeled as Option 11 for Item 2 of Card Series 1XX400. This resulted in the use of a user specified heat transfer coefficient entered in Card Series 420001. In Calculation N-4080-002 (page 193) a heat sink to containment sump water heat transfer coefficient of 0.4 BTU/hr-ft2-oF was specified. This same heat transfer coefficient value is available as Option 3 for Item 2 of Card Series 1XX400. To negate the need for input for Card Series 420001, in this calculation the heat transfer coefficient control for the left boundary condition is modeled as Option 3 for Item 2 of Card Series 1XX400.

Because there is no heat transfer across the right boundary, the bulk temperature control for the right boundary condition is not used by the COPATTA Code. Therefore, in this analysis the bulk temperature control for the right boundary condition is modeled as the containment liquid temperature (i.e., Option 3 for Item 5 of Card Series 1XX400). This differs from the modeling of Calculation N-4080-002, which employed Option 0 for Item 5 of Card Series 1XX400. Since the bulk temperature control for the right boundary condition has no meaning for this Heat Sink, the decision to model Item 5 with Option 3 rather than Option 0 has the beneficial consequence of allowing the use of any positive value to be modeled as the variable TCONT in Item 7 of Card Series 2.

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The Card Series set defining Heat Sink 5 is entered in the input data file as:

* HS #5 - REACTOR BASEMAT & S.G. PEDESTALS &LIST POOL=105201, 70, 4, 0, 0, 0, 0, 1644/ &LIST POOL=105101, 4, 0.00158, 10, 0.1, 30, 2.00, 25, 8.43092/ &LIST POOL=105201, 4, 2, 2, 2/ &LIST POOL=105300, 0, 0/ &LIST FOOL=105400, 3, 3, 0, 3/

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8.1.27.6 HS #6 - Reactor Cavity Walls below El. 15'0"

The characteristics of the Reactor Cavity Walls below plant elevation 15'0" are as determined in Calculation N-4080-002 (Reference 6.1.g, pages 142 through 144) for Heat Sink 6.

Heat Sink #6 describes the Reactor Cavity Walls below El. 15'0" as modeled:

11.75 ft
21.5 ft
1590 ft ²
0.00192 ft (= 0.023 in)
13.5 ft (= 162 in)
Exposed to containment sump water
Insulated, no heat transfer to the ground on the opposite side of the walls

Due to an addition error, Calculation N-4080-002 (page 143) incorrectly modeled the right boundary coordinate of the Concrete Region at 25.25 feet. The determination of the right boundary coordinate of the Concrete region was based on adding the thickness of the Concrete Region to the inside radius of the cylinder model, and neglecting to add the thickness of the Organic Paint Region. In this analysis the right boundary coordinate of the Concrete Region will be modeled at the correct position of 25.25192 feet:

Right Boundary Coordinate of Concrete Region = 11.75 ft + 0.00192 ft + 13.5 ft= 25.25192 feet

In Calculation N-4080-002 (page 198) the cylinder height was incorrectly entered into the COPATTA Code input file as 8.5 feet, rather than the 21.5 feet value calculated on page 143. In this analysis the cylinder height will be modeled as 21.5 feet.

In Calculation N-4080-002 (page 144) the heat transfer coefficient control for the left boundary condition was modeled as Option 11 for Item 2 of Card Series 1XX400. This

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resulted in the use of a user specified heat transfer coefficient entered in Card Series 420001. In Calculation N-4080-002 (page 193) a heat sink to containment sump water heat transfer coefficient of 0.4 BTU/hr-ft²-°F was specified. This same heat transfer coefficient value is available as Option 3 for Item 2 of Card Series 1XX400. To negate the need for input for Card Series 420001, in this calculation the heat transfer coefficient control for the left boundary condition is modeled as Option 3 for Item 2 of Card Series 1XX400.

Because there is no heat transfer across the right boundary, the bulk temperature control for the right boundary condition is not used by the COPATTA Code. Therefore, in this analysis the bulk temperature control for the right boundary condition is modeled as the containment liquid temperature (i.e., Option 3 for Item 5 of Card Series 1XX400). This differs from the modeling of Calculation N-4080-002, which employed Option 0 for Item 5 of Card Series 1XX400. Since the bulk temperature control for the right boundary condition has no meaning for this Heat Sink, the decision to model Item 5 with Option 3 rather than Option 0 has the beneficial consequence of allowing the use of any positive value to be modeled as the variable TCONT in Item 7 of Card Series 2.

The Card Series set defining Heat Sink 6 is entered in the input data file as:

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8.1.27.7 HS #7 - Reactor Cavity Walls above El. 15'0"

The characteristics of the Reactor Cavity Walls above plant elevation 15'0" are as determined in Calculation N-4080-002 (Reference 6.1.g), pages 144 through 146) for Heat Sink 7.

Due to heat sink symmetry, only one-half of the heat sink is modeled. The modeled surface area is the total heat sink surface area, equal to twice the actual surface area of one side of the heat sink. The modeled thickness of the center concrete portion is one-half of the actual thickness of the center concrete portion of the heat sink. And, the modeled outside boundary is the adiabatic (insulated) condition existing at the midplane of the symmetrical heat sink.

Heat Sink #7 describes the Reactor Cavity Walls above El. 15'0" as modeled:

Geometry Slab

Surface Area 2810 ft²

Organic Paint (material 4) thickness-Left 0.00192 ft (= 0.023 in)

Boundary

Concrete (material 2) thickness-Right Boundary 4.00 ft (= 48 in)

Left Boundary condition Exposed to containment atmosphere

Right Boundary condition Insulated, no heat transfer is modeled across the heat sink

centerline

Because there is no heat transfer across the right boundary, the bulk temperature control for the right boundary condition is not used by the COPATTA Code. Therefore, in this analysis the bulk temperature control for the right boundary condition is modeled as the containment vapor temperature for convective heat transfer or the saturation temperature at the containment steam partial pressure for condensing heat transfer (i.e., Option 2 for Item 5 of Card Series 1XX400). This differs from the modeling of Calculation N-4080-002, which employed Option 0 for Item 5 of Card Series 1XX400. Since the bulk temperature control for the right boundary condition has no meaning for this Heat Sink, the decision to model Item 5 with Option 2 rather than Option 0 has the beneficial consequence of allowing the use of any positive value to be modeled as the variable TCONT in Item 7 of Card Series 2.

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The Card Series set defining Heat Sink 7 is entered in the input data file as:

```
* HS #7 - REACTOR CAVITY WALLS ABOVE E1. 15'0"
 &LIST POOL=107001, 68, 5, 0, 0, 0, 0, 2810/
&LIST POOL=107101, 5, 0.00192, 7, 0.02292,
15, 0.40192, 20, 2.00,
20, 4.00192/
 &LIST POOL=107201, 4, 2, 2, 2, 2/
 &LIST POOL=107300, 0, 0/
 &LIST POOL=107400, 9, 2, 0, 2/
```

As discussed in Design Input 4.8, the heat transfer coefficient control for the left boundary condition (adjacent to the organic paint) is modeled as the Uchida value. This is a condensing steam value dependent on the ratio of water vapor to air used in MSLB analyses. Therefore Item 2 in Card Series 107400 is 9.

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8.1.27.8 HS #8 - Lined Refueling Canal Walls

The characteristics of the Lined Refueling Canal Walls are as determined in Calculation N-4080-002 (Reference 6.1.g), pages 146 through 149) for Heat Sink 8.

Heat Sink #8 describes the Lined Refueling Canal Walls as modeled:

Geometry Slab Surface Area 9200 ft²

Stainless Steel (material 3) thickness-Left 0.01563 ft (= 0.1875 in)

Boundary

Concrete (material 2) thickness 4.00 ft (= 48 in)

Organic Paint (material 4) thickness-Right 0.00192 ft (= 0.023 in)

Boundary

Left Boundary condition Exposed to containment atmosphere

Right Boundary condition Exposed to containment atmosphere

The Card Series set defining Heat Sink 8 is entered in the input data file as:

```
* HS #8 - LINED REFUELING CANAL WALLS
 &LIST POOL=108001, 86, 6, 0, 0, 0, 0, 9200/
&LIST POOL=108101, 5, 0.01563, 20, 15, 0.41563, 20, 20, 4.01563, 5,
                                                    0.1,
                       20, 4.01563,
                                          5, 4.01755/
 &LIST POOL=108201, 3, 2, 2, 2, 2, 4/
&LIST POOL=108300, 0, 0/
&LIST POOL=108400, 9, 2, 9, 2/
```

As discussed in Design Input 4.8, the heat transfer coefficient control for the left and right boundary conditions are modeled as the Uchida value. This is a condensing steam value dependent on the ratio of water vapor to air used in MSLB analyses. Therefore Items 2 and 4 in Card Series 108400 are 9.

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8.1.27.9 HS #9 - Steam Generator Compartment Walls, Unlined Refueling Canal Walls above El. 63'6", and Other Interior Walls

The characteristics of the Steam Generator Compartment Walls, Unlined Refueling Canal Walls above plant elevation 63'6", and Other Interior Walls are as determined in Calculation N-4080-002 (Reference 6.1.g), pages 149 through 152) for Heat Sink 9.

Due to heat sink symmetry, only one-half of the heat sink is modeled. The modeled surface area is the total heat sink surface area, equal to twice the actual surface area of one side of the heat sink. The modeled thickness of the center concrete portion is one-half of the actual thickness of the center concrete portion of the heat sink. And, the modeled outside boundary is the adiabatic (insulated) condition existing at the midplane of the symmetrical heat sink.

Heat Sink #9 describes the Steam Generator Compartment Walls, Unlined Refueling Canal Walls above El. 63'6", and Other Interior Walls as modeled:

Slab

Geometry

Surface Area 41976 ft²

Organic Paint (material 4) thickness-Left 0.00192 ft (= 0.023 in)

Boundary

Concrete (material 2) thickness-Right Boundary 1.71684 ft

Left Boundary condition Exposed to containment atmosphere

Right Boundary condition Insulated, no heat transfer across

the heat sink centerline

Because there is no heat transfer across the right boundary, the bulk temperature control for the right boundary condition is not used by the COPATTA Code. Therefore, in this analysis the bulk temperature control for the right boundary condition is modeled as the containment vapor temperature for convective heat transfer or the saturation temperature at the containment steam partial pressure for condensing heat transfer (i.e., Option 2 for Item 5 of Card Series 1XX400). This differs from the modeling of Calculation N-4080-002, which employed Option 0 for Item 5 of Card Series 1XX400. Since the bulk temperature control for the right boundary condition has no meaning for this Heat Sink, the decision to model Item 5 with Option 2 rather than Option 0 has the beneficial consequence of allowing the use of any positive value to be modeled as the variable TCONT in Item 7 of Card Series 2.

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The Card Series set defining Heat Sink 9 is entered in the input data file as:

* HS #9 - S.G. CMPRTMNT WALLS, UNLINED REFL CNL WALLS/OTH INT WALLS &LIST POOL=109001, 78, 4, 0, 0, 0, 0, 41976/ &LIST POOL=109101, 5, 0.00192, 10, 0.04233, 12, 0.1, 50, 1.71876/ \$\frac{12}{\text{ 0.1,}} \tag{6.1}, \\ \text{&LIST POOL=109201, 4, 2, 2, 2/} \\ \text{&LIST POOL=109300, 0, 0/} \end{array} &LIST POOL=109400, 9, 2, 0, 2/

As discussed in Design Input 4.8, the heat transfer coefficient control for the left boundary condition (adjacent to the organic paint) is modeled as the Uchida value. This is a condensing steam value dependent on the ratio of water vapor to air used in MSLB analyses. Therefore Item 2 in Card Series 109400 is 9.

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8.1.27.10 HS #10 - Floor Slabs (other than basemats)

The characteristics of the Floor Slabs (other than basemats) represent a refinement of the characteristics as determined in Calculation N-4080-002 (pages 152 through 155) for Heat Sink 10.

Heat Sink #10 describes Floor Slabs (other than basemats) as modeled:

Geometry Slab

Surface Area 17474 ft²

Organic Paint #1 (material 4) thickness-Left 0.00014 ft

Boundary

Carbon Steel (material 1) thickness 0.005208 ft (= 0.0625 in)

Concrete (material 2) thickness 1.5 ft

Organic Paint #2 (material 4) thickness-Right 0.000667 ft (= 0.008 in)

Boundary

Right Boundary condition Exposed to containment atmosphere

The 17474 square foot surface area of the floor slabs modeled in this analysis is equivalent to the concrete side surface area given in Calculation C-257-1.96.01 (Reference 6.1.a, pages 15 and 26). The same calculation gives a metal decking are of 23,240 square feet (page 26). The higher area is due to the metal decking which is corrugated steel while the smaller area is the area of the concrete slab under it. The smaller area of 17474 square foot will be conservatively used here.

Calculation N-4080-002 (Reference 6.1.g, page 152) used a value of 17172 square feet and is based on input data provided as Attachment 1 to Calculation N-4080-002 (page 328). This surface area differs from that described in Calculation N-4080-005 (Reference 6.1.f, page 42), which attempted to refine the floor slab heat sink model by increasing the surface area of the floor slab from 17172 to 23240 square feet. Although the area was to be increased, the actual COPATTA Code runs of Calculation N-4080-005 continued to model the original smaller floor slab surface area of 17172 square feet.

As discussed in Design Input Item 4.8.k, when the nodalization of the Concrete Region was performed, Calculation N-4080-002 (page 153) modeled the concrete as Heat Sink 10 Regions 3, 4 and 5, with a total concrete thickness of 2.0 feet rather than 1.5 feet. To

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model the correct concrete thickness requires that the Region 5 thickness be reduced by 0.5 feet. This is accomplished by shifting the right boundary of Region 5 to the left by 0.5 feet. As a consequence, the right boundary of Region 6 (the second Organic Paint layer) must also be shifted to the left by 0.5 feet. The changes from the right boundary locations determined in Calculation N-4080-002 are:

1st Region: no change in the right boundary location no change in the right boundary location 2nd Region: no change in the right boundary location 3rd Region: 4th Region: no change in the right boundary location

5th Region: right boundary shifted from 2.005348 to 1.505348 feet 6th Region: right boundary shifted from 2.006015 to 1.506015 feet

The Card Series set defining Heat Sink 10 is entered in the input data file as:

```
* HS #10 - FLOOR SLABS (OTHER THAN BASEMATS)
 &LIST POOL=110001, 67, 6, 0, 0, 0, 0, 17474/
 &LIST POOL=110101, 3, 0.00014, 5, 0.005348, 20, 0.105348, 15, 0.505348, 20, 1.505348, 3, 1.506015/
 &LIST POOL=110300, 0, 0/
 &LIST POOL=110400 9, 2, 9, 2/
```

As discussed in Design Input 4.8, the heat transfer coefficient control for the left and right boundary conditions are modeled as the Uchida value. This is a condensing steam value dependent on the ratio of water vapor to air used in MSLB analyses. Therefore Items 2 and 4 in Card Series 110400 are 9.

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8.1.27.11 HS #11 - Lifting Devices (except stainless steel parts)

The characteristics of the Lifting Devices (except stainless steel parts) are as determined in Calculation N-4080-005 (Reference 6.1.f, pages 42 through 44) for Heat Sink 10. This heat sink description represents a refinement of the characteristics of the Lifting Devices first determined in Calculation N-4080-002 (Reference g.1.g, pages 156 through 158) for Heat Sink 11.

Due to heat sink symmetry, only one-half of the heat sink is modeled. The modeled surface area is the total heat sink surface area, equal to twice the actual surface area of one side of the heat sink. The modeled thickness of the center carbon steel portion is one-half of the actual thickness of the center carbon steel portion of the heat sink. And, the modeled outside boundary is the adiabatic (insulated) condition existing at the midplane of the symmetrical heat sink.

Heat Sink #11 describes the Lifting Devices (except stainless steel parts) as modeled:

Geometry Slab Surface Area 57286 ft²

Organic Paint (material 4) thickness-Left 0.00125 ft (= 0.015 in)

Boundary

Carbon Steel (material 1) thickness-Right 0.041667 ft

Boundary

Left Boundary condition Exposed to containment atmosphere

Right Boundary condition Insulated, no heat transfer across

the heat sink centerline

Because there is no heat transfer across the right boundary, the bulk temperature control for the right boundary condition is not used by the COPATTA Code. Therefore, in this analysis the bulk temperature control for the right boundary condition is modeled as the containment vapor temperature for convective heat transfer or the saturation temperature at the containment steam partial pressure for condensing heat transfer (i.e., Option 2 for Item 5 of Card Series 1XX400). This differs from the modeling of Calculation N-4080-002, which employed Option 0 for Item 5 of Card Series 1XX400. Since the bulk temperature control for the right boundary condition has no meaning for this Heat Sink, the decision to model Item 5 with Option 2 rather than Option 0 has the beneficial consequence of allowing the use of any positive value to be modeled as the variable TCONT in Item 7 of Card Series 2.

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The Card Series set defining Heat Sink 11 is entered in the input data file as:

* HS #11 - LIFTING DEVICES (EXCEPT STAINLESS STEEL PARTS) &LIST POOL=111001, 17, 2, 0, 0, 0, 0, 57286/ &LIST POOL=111101, 6, 0.00125, 10, 0.042917/ &LIST POOL=111201, 4, 1/ &LIST POOL=111300, 0, 0/ &LIST POOL=111400, 9, 2, 0, 2/

As discussed in Design Input 4.8, the heat transfer coefficient control for the left boundary condition (adjacent to the organic paint) is modeled as the Uchida value. This is a condensing steam value dependent on the ratio of water vapor to air used in MSLB analyses. Therefore Item 2 in Card Series 111400 is 9.

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8.1.27.12 HS #12 - Miscellaneous Carbon Steel (with thickness greater than 2.50 in)

The characteristics of the Miscellaneous Carbon Steel (with thickness greater than 2.50 in) are as determined in Calculation N-4080-005 (Reference 6.1.f, pages 44 through 47) for Heat Sink 11. This heat sink description represents a refinement of the characteristics of the Miscellaneous Carbon Steel first determined in Calculation N-4080-002 (Reference 6.1.g. pages 58 through 161) for Heat Sink 12.

Due to heat sink symmetry, only one-half of the heat sink is modeled. The modeled surface area is the total heat sink surface area, equal to twice the actual surface area of one side of the heat sink. The modeled thickness of the center carbon steel portion is one-half of the actual thickness of the center carbon steel portion of the heat sink. And, the modeled outside boundary is the adiabatic (insulated) condition existing at the midplane of the symmetrical heat sink.

Heat Sink #12 describes the Miscellaneous Carbon Steel (with thickness greater than 2.50 in) as modeled:

Geometry	Slab
Surface Area	516 ft ²
Organic Paint (material 4) thickness-Left Boundary	0.0005 ft (= 0.006 in)
Carbon Steel (material 1) thickness-Right Boundary	0.310349 ft
Left Boundary condition	Exposed to containment atmosphere
Right Boundary condition	Insulated, no heat transfer across the heat sink centerline

Calculation N-4080-005 (page 44) calculates a Miscellaneous Carbon Steel surface area of 516 square feet. However, due to an apparent transcription error, a surface area of 596 square feet was modeled in the Calculation N-4080-005 COPATTA Code input files. This calculation will model the calculated area of 516 square feet.

Calculation N-4080-005 (page 45) calculates a right boundary coordinate of 0.310849 feet for the Carbon Steel Region. However, for unknown reasons, a right boundary coordinate of 0.34414 feet was modeled in the Calculation N-4080-005 COPATTA Code input files. This calculation will model the calculated right boundary coordinate of 0.310849 feet for the Carbon Steel Region.

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Because there is no heat transfer across the right boundary, the bulk temperature control for the right boundary condition is not used by the COPATTA Code. Therefore, in this analysis the bulk temperature control for the right boundary condition is modeled as the containment vapor temperature for convective heat transfer or the saturation temperature at the containment steam partial prossure for condensing heat transfer (i.e., Option 2 for Item 5 of Card Series 1XX400). This differs from the modeling of Calculations N-4080-002 and N-4080-005, which employed Option 0 for Item 5 of Card Series 1XX400. Since the bulk temperature control for the right boundary condition has no meaning for this Heat Sink, the decision to model Item 5 with Option 2 rather than Option 0 has the beneficial consequence of allowing the use of any positive value to be modeled as the variable TCONT in Item 7 of Card Series 2.

The Card Series set defining Heat Sink 12 is entered in the input data file as:

```
* HS #12 - MISCELLANEOUS CARBON STEEL - THICKNESS > 2.50 INCHES &LIST POOL=112001, 64, 4, 0, 0, 0, 0, 516/ &LIST POOL=112101, 6, 0.0005, 17, 0.084, 15, 0.20, 25, 0.310849/ &LIST POOL=112201, 4, 1, 1, 1/ &LIST POOL=112300, 0, 0/ &LIST POOL=112400, 9, 2, 0, 2/
```

As discussed in Design Input 4.8, the heat transfer coefficient control for the left boundary condition (adjacent to the organic paint) is modeled as the Uchida value. This is a condensing steam value dependent on the ratio of water vapor to air used in MSLB analyses. Therefore Item 2 in Card Series 112400 is 9.

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8.1.27.13 HS #13 - Miscellaneous Carbon Steel (with thickness between 1.00 in and 2.50 in)

The characteristics of the Miscellaneous Carbon Steel (with thickness between 1.00 in and 2.50 in) are as determined in Calculation N-4080-005 (Reference 6.1.f, pages 47 through 50) for Heat Sink 12. This heat sink description represents a refinement of the characteristics of the Miscellaneous Carbon Steel first determined in Calculation N-4080-002 (Reference 6.1.g, pages 161 through 165) for Heat Sink 13.

An error was made in Calculation N-4080-005 for Heat Sink 12 on page 48. There are four Safety Injections Tanks and the area of only one tank was modeled by Calculation N-4080-005. Correcting this error will change the surface area for Heat Sink 13 in this analysis to 12042 square feet and the effective carbon steel thickness to 0.1692 feet.

Due to heat sink symmetry, only one-half of the heat sink is modeled. The modeled surface area is the total heat sink surface area, equal to twice the actual surface area of one side of the heat sink. The modeled thickness of the center carbon steel portion is one-half of the actual thickness of the center carbon steel portion of the heat sink. And, the modeled outside boundary is the adiabatic (insulated) condition existing at the midplane of the symmetrical heat sink.

Heat Sink #13 describes the Miscellaneous Carbon Steel (with thickness between 1.00 in and 2.50 in) as modeled:

Geometry	Slab
Surface Area	12042 ft ²
Organic Paint (material 4) thickness-Left Boundary	0.00063 ft
Carbon Steel (material 1) thickness-Right Boundary	0.16924 ft
Left Boundary condition	Exposed to containment atmosphere
Right Boundary condition	Insulated, no heat transfer across the heat sink centerline

Because there is no heat transfer across the right boundary, the bulk temperature control for the right boundary condition is not used by the COPATTA Code. Therefore, in this analysis the bulk temperature control for the right boundary condition is modeled as the containment vapor temperature for convective heat transfer or the saturation temperature at the containment steam partial pressure for condensing heat transfer (i.e., Option 2 for Item 5 of

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Card Series 1XX400). This differs from the modeling of Calculations N-4080-002 and N-4080-005, which employed Option 0 for Item 5 of Card Series 1XX400. Since the bulk temperature control for the right boundary condition has no meaning for this Heat Sink, the decision to model Item 5 with Option 2 rather than Option 0 has the beneficial consequence of allowing the use of any positive value to be modeled as the variable TCONT in Item 7 of Card Series 2.

The Card Series set defining Heat Sink 13 is entered in the input data file as:

* HS #13 - MISCELLANEOUS CARBON STEEL: 1.00"<THICKNESS<2.50"
&LIST POOL=113001, 32, 2, 0, 0, 0, 0, 12042/
&LIST POOL=113101, 6, 0.00063, 25, 0.16967/
&LIST POOL=113201, 4, 1/
&LIST POOL=113300, 0, 0/
&LIST POOL=113400, 9, 2, 0, 2/

As discussed in Design Input 4.8, the heat transfer coefficient control for the left boundary condition (adjacent to the organic paint) is modeled as the Uchida value. This is a condensing steam value dependent on the ratio of water vapor to air used in MSLB analyses. Therefore Item 2 in Card Series 113400 is 9.

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8.1.27.14 HS #14 - Miscellaneous Carbon Steel (with thickness between 0.50 in and 1.00 in)

The characteristics of the Miscellaneous Carbon Steel (with thickness between 0.50 in and 1.00 in) are as determined in Calculation N-4080-005 (Reference 6.1.f, pages 50 through 54) for Heat Sink 13. This heat sink description represents a refinement of the characteristics of the Miscellaneous Carbon Steel first determined in Calculation N-4080-002 (Reference 6.1.g, pages 165 through 169) for Heat Sink 14.

Due to heat sink symmetry, only one-half of the heat sink is modeled. The modeled surface area is the total heat sink surface area, equal to twice the actual surface area of one side of the heat sink. The modeled thickness of the center carbon steel portion is one-half of the actual thickness of the center carbon steel portion of the heat sink. And, the modeled outside boundary is the adiabatic (insulated) condition existing at the midplane of the symmetrical heat sink.

Heat Sink #14 describes the Miscellaneous Carbon Steel (with thickness between 0.50 in and 1.00 in) as modeled:

Geometry	Slab
Surface Area	64693 ft ²
Organic Paint (material 4) thickness-Left Boundary	0.000674 ft
Carbon Steel (material 1) thickness-Right Boundary	0.037933 ft
Left Boundary condition	Exposed to containment atmosphere
Right Boundary condition	Insulated, no heat transfer across the heat sink centerline

Because there is no heat transfer across the right boundary, the bulk temperature control for the right boundary condition is not used by the COPATTA Code. Therefore, in this analysis the bulk temperature control for the right boundary condition is modeled as the containment vapor temperature for convective heat transfer or the saturation temperature at the containment steam partial pressure for condensing heat transfer (i.e., Option 2 for Item 5 of Card Series 1XX400). This differs from the modeling of Calculations N-4080-002 and N-4080-005, which employed Option 0 for Item 5 of Card Series 1XX400. Since the bulk temperature control for the right boundary condition has no meaning for this Heat Sink, the decision to model Item 5 with Option 2 rather than Option 0 has the beneficial consequence

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of allowing the use of any positive value to be modeled as the variable TCONT in Item 7 of Card Series 2.

The Card Series set defining Heat Sink 14 is entered in the input data file as:

```
* HS #14 - MISCELLANEOUS CARBON STEEL: 0.50"<THICKNESS<1.00"
 &LIST POOL=114001, 19, 2, 0, 0, 0, 0, 64693/
&LIST POOL=114101, 5, 0.000674, 13, 0.038607/
 &LIST POOL=114201, 4, 1/
 &LIST POOL=114300, 0, 0/
 &LIST POOL=114400, 9, 2, 0, 2/
```

As discussed in Design Input 4.8, the heat transfer coefficient control for the left boundary condition (adjacent to the organic paint) is modeled as the Uchida value. This is a condensing steam value dependent on the ratio of water vapor to air used in MSLB analyses. Therefore Item 2 in Card Series 114400 is 9.

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8.1.27.15 HS #15 - Miscellaneous Carbon Steel (with thickness less than 0.50 in)

The characteristics of the Miscellaneous Carbon Steel (with thickness less than 0.50 in) are as determined in Calculation N-4080-005 (Reference 6.1.f, pages 54 through 59) for Heat Sink 14. This heat sink description represents a refinement of the characteristics of the Miscellaneous Carbon Steel first determined in Calculation N-4080-002 (Reference 6.1.g, pages 169 through 173) for Heat Sink 15.

Due to heat sink symmetry, only one-half of the heat sink is modeled. The modeled surface area is the total heat sink surface area, equal to twice the actual surface area of one side of the heat sink. The modeled thickness of the center carbon steel portion is one-half of the actual thickness of the center carbon steel portion of the heat sink. And, the modeled outside boundary is the adiabatic (insulated) condition existing at the midplane of the symmetrical heat sink.

Heat Sink #15 describes the Miscellaneous Carbon Steel (with thickness less than 0.50 in as modeled:

Geometry	Slab
Surface Area	98913.6 ft ²
Organic Paint (material 4) thickness-Left Boundary	0.000606 ft
Carbon Steel (material 1) thickness-Right Boundary	0.012227 ft
Left Boundary condition	Exposed to containment atmosphere
Right Boundary condition	Insulated, no heat transfer across the heat sink centerline

Because there is no heat transfer across the right boundary, the bulk temperature control for the right boundary condition is not used by the COPATTA Code. Therefore, in this analysis the bulk temperature control for the right boundary condition is modeled as the containment vapor temperature for convective heat transfer or the saturation temperature at the containment steam partial pressure for condensing heat transfer (i.e., Option 2 for Item 5 of Card Series 1XX400). This differs from the modeling of Calculations N-4080-002 and N-4080-005, which employed Option 0 for Item 5 of Card Series 1XX400. Since the bulk temperature control for the right boundary condition has no meaning for this Heat Sink, the decision to model Item 5 with Option 2 rather than Option 0 has the beneficial consequence

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of allowing the use of any positive value to be modeled as the variable TCONT in Item 7 of Card Series 2.

The Card Series set defining Heat Sink 15 is entered in the input data file as:

```
* HS #15 - MISCELLANEOUS CARBON STEEL: THICKNESS<0.5"
 &LIST POOL=115001, 17, 2, 0, 0, 0, 0, 98913.6/
&LIST POOL=115101, 6, 0.000606, 10, 0.012833/
 &LIST POOL=115201, 4, 1/
 &LIST POOL=115300, 0, 0/
 &LIST POOL=115400, 9, 2, 0, 2/
```

As discussed in Design Input 4.8, the heat transfer coefficient control for the left boundary condition (adjacent to the organic paint) is modeled as the Uchida value. This is a condensing steam value dependent on the ratio of water vapor to air used in MSLB analyses. Therefore Item 2 in Card Series 115400 is 9.

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8.1.27.16 HS #16 - Electrical Equipment

The characteristics of the Electrical Equipment are as determined in Calculation N-4080-005 (Reference 6.1.f, pages 59 through 61) for Heat Sink 15. This heat sink description represents a refinement of the characteristics of the Electrical Steel first determined in Calculation N-4080-002 (Reference 6.1.g, pages 174 through 176) for Heat Sink 16.

Calculation N-4080-005 (page 61) recommends use of a 37644 square foot surface area. The modeled surface area of 37644.5 square feet possesses the extra significant digit found in an interim calculation step as shown in Calculation N-4080-005 (page 60).

Heat Sink #16 describes the Electrical Equipment as modeled:

Geometry

Slab

Surface Area

37644.5 ft²

Carbon Steel (material 1) thickness-Left and

0.0054 ft

Right boundaries

Left Boundary condition

Exposed to containment atmosphere

Right Boundary condition

Insulated, no heat transfer to inside

of electrical equipment

Because there is no heat transfer across the right boundary, the bulk temperature control for the right boundary condition is not used by the COPATTA Code. Therefore, in this analysis the bulk temperature control for the right boundary condition is modeled as the containment vapor temperature for convective heat transfer or the saturation temperature at the containment steam partial pressure for condensing heat transfer (i.e., Option 2 for Item 5 of Card Series 1XX400). This differs from the modeling of Calculations N-4080-002 and N-4080-005, which employed Option 0 for Item 5 of Card Series 1XX400. Since the bulk temperature control for the right boundary condition has no meaning for this Heat Sink, the decision to model Item 5 with Option 2 rather than Option 0 has the beneficial consequence of allowing the use of any positive value to be modeled as the variable TCONT in Item 7 of Card Series 2.

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The Card Series set defining Heat Sink 16 is entered in the input data file as:

```
* HS #16 - ELECTRICAL EQUIPMENT
 &LIST POOL=116001, 8, 1, 0, 0, 0, 0, 37644.5/
&LIST POOL=116101, 7, 0.0054/
&LIST POOL=116201, 1/
 &LIST POOL=116300, 0, 0/
 &LIST POOL=116400, 9, 2, 0, 2/
```

As discussed in Design Input 4.8, the heat transfer coefficient control for the left boundary condition (adjacent to the organic paint) is modeled as the Uchida value. This is a condensing steam value dependent on the ratio of water vapor to air used in MSLB analyses. Therefore Item 2 in Card Series 116400 is 9.

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8.1.27.17 HS #17 - Miscellaneous Stainless Steel

The characteristics of the Miscellaneous Stainless Steel are as determined in Calculation N-4080-005 (Reference 6.1.f, pages 62 through 65) for Heat Sink 16. This heat sink description represents a refinement of the characteristics of the Miscellaneous Stainless Steel as first determined in Calculation N-4080-002 (Reference 6.1.g, pages 176 through 179) for Heat Sink 17.

Due to heat sink symmetry, only one-half of the heat sink is modeled. The modeled surface area is the total heat sink surface area, equal to twice the actual surface area of one side of the heat sink. The modeled thickness of the center stainless steel portion is one-half of the actual thickness of the center stainless steel portion of the heat sink. And, the modeled outside boundary is the adiabatic (insulated) condition existing at the midplane of the symmetrical heat sink.

Heat Sink #17 describes the Miscellaneous Stainless Steel as modeled:

Geometry Slab

Surface Area 24048 ft²

Stainless Steel (material 3) thickness-Left and 0.01747 ft

Right boundaries

Left Boundary condition Exposed to containment atmosphere

Right Boundary condition Insulated, no heat transfer across

the heat sink centerline

Because there is no heat transfer across the right boundary, the bulk temperature control for the right boundary condition is not used by the COPATTA Code. Therefore, in this analysis the bulk temperature control for the right boundary condition is modeled as the containment vapor temperature for convective heat transfer or the saturation temperature at the containment steam partial pressure for condensing heat transfer (i.e., Option 2 for Item 5 of Card Series 1XX400). This differs from the modeling of Calculations N-4080-002 and N-4080-005, which employed Option 0 for Item 5 of Card Series 1XX400. Since the bulk temperature control for the right boundary condition has no meaning for this Heat Sink, the decision to model Item 5 with Option 2 rather than Option 0 has the beneficial consequence of allowing the use of any positive value to be modeled as the variable TCONT in Item 7 of Card Series 2.

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The Card Series set defining Heat Sink 17 is entered in the input data file as:

* HS #17 - MISCELLANEOUS STAINLESS STEEL &LIST POOL=117001, 16, 1, 0, 0, 0, 0, 24048/ &LIST POOL=117101, 15, 0.01747/ &LIST POOL=117201, 3/ &LIST POOL=117300, 0, 0/ &LIST POOL=117400, 9, 2, 0, 2/

As discussed in Design Input 4.8, the heat transfer coefficient control for the left boundary condition (adjacent to the organic paint) is modeled as the Uchida value. This is a condensing steam value dependent on the ratio of water vapor to air used in MSLB analyses. Therefore Item 2 in Card Series 117400 is 9.

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8.1.27.18 HS #18 - Unlined Refueling Canal Walls (below El. 63'6")

The characteristics of the Unlined Refueling Canal Walls (below plant elevation 63'6") are as determined in Calculation N-4080-002 (Reference 6.1.g, pages 180 through 182) for Heat Sink 18.

Due to heat sink symmetry, only one-half of the heat sink is modeled. The modeled surface area is the total heat sink surface area, equal to twice the actual surface area of one side of the heat sink. The modeled thickness of the center concrete portion is one-half of the actual thickness of the center concrete portion of the heat sink. And, the modeled outside boundary is the adiabatic (insulated) condition existing at the midplane of the symmetrical heat sink.

Heat Sink #18 describes the Unlined Refueling Canal Walls (below El. 63'6") as modeled:

Geometry Slab

Surface Area 3700 ft²

Organic Paint (material 4) thickness-Left 0.00192 ft (= 0.023 in)

Boundary

Concrete (material 2) thickness-Right Boundary 2.0 ft

Left Boundary condition Exposed to containment atmosphere

Right Boundary condition Insulated, no heat transfer across

the heat sink centerline

Due to an addition error, Calculation N-4080-002 (page 181) incorrectly modeled the right boundary coordinate of the Concrete Region at 2.00 feet. The determination of the right boundary coordinate of the Concrete region neglected to add the thickness of the Organic Paint Region. In this analysis the right boundary coordinate of the Concrete Region will be modeled at the correct position of 2.00192 feet:

Right Boundary Coordinate of Concrete Region = 2.0 ft + 0.00192 ft

= 2.00192 feet

Because there is no heat transfer across the right boundary, the bulk temperature control for the right boundary condition is not used by the COPATTA Code. Therefore, in this analysis the bulk temperature control for the right boundary condition is modeled as the containment vapor temperature for convective heat transfer or the saturation temperature at the containment steam partial pressure for condensing heat transfer (i.e., Option 2 for Item 5 of Card Series 1XX400). This differs from the modeling of Calculation N-4080-002, which

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employed Option 0 for Item 5 of Card Series 1XX400. Since the bulk temperature control for the right boundary condition has no meaning for this Heat Sink, the decision to model Item 5 with Option 2 rather than Option 0 has the beneficial consequence of allowing the use of any positive value to be modeled as the variable TCONT in Item 7 of Card Series 2.

The Card Series set defining Heat Sink 18 is entered in the input data file as:

```
* HS #18 - UNLINED REFUELING CANAL WALLS BELOW E1. 63'6"
 &LIST POOL=118001, 48, 4, 0, 0, 0, 0, 3700/
&LIST POOL=118101, 5, 0.00192, 15, 0.40192,
                                        7, 0.02292,
20, 2.00192/
&LIST POOL=118201, 4, 2, 2, 2/
&LIST POOL=118300, 0, 0/
 &LIST POOL=118400, 9, 2, 0, 2/
```

As discussed in Design Input 4.8, the heat transfer coefficient control for the left boundary condition (adjacent to the organic paint) is modeled as the Uchida value. This is a condensing steam value dependent on the ratio of water vapor to air used in MSLB analyses. Therefore Item 2 in Card Series 118400 is 9.

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8.1.27.19 HS #19 - Reactor Building Cylinder #3 (the Containment Section with Embedded Stiffeners between El. 29'6" and 112'0")

The characteristics of the Reactor Building Cylinder #3 (the Containment Section with Embedded Stiffeners between plant elevations 29'6" and 112'0") are as determined in Calculation N-4080-002 (Reference 6.1.f, pages 183 through 189) for Heat Sink 19, except for the thickness of the Containment Liner/Concrete air gap interface, and except for the thickness of the concrete layer.

Due to an addition error, Calculation N-4080-002 (page 188) improperly modeled the concrete layer as 3.56524 feet thick. In this analysis the concrete layer will be modeled as 4.21108 feet, corresponding to the average thickness that was actually determined in Calculation N-4080-002 (page 186). And, as discussed in Design Input Item 4.8.a, the effective thickness of the interface (air gap) will be 0.00035 feet. With these changes, Heat Sink #19 describes the Reactor Building Cylinder 3 as modeled:

Geometry Slab

Surface Area 1590.68 ft²

Organic Paint (material 4) thickness-Left 0.00075 ft (= 0.009 in)

Boundary

Carbon Steel (material 1) Liner thickness 0.66667 ft (= 8 in)

Air Gap Interface (material 5) thickness 0.00035 ft Concrete (material 2) thickness-Right Boundary 4.21108 ft

Left Boundary condition Exposed to containment atmosphere

Right Boundary condition Exposed to outside environment

The effect of the changes in the air gap thickness is reflected in Card Series 119101. This Card Series defines the location of the right boundary and nodalization of each region. The air gap is the third region of Heat Sink 19. The increase in the modeled air gap thickness from 0.00017 feet to 0.00035 feet requires that the modeled location of the Region 3 right boundary be increased by 0.00018 feet. To maintain the correct thickness of each Region that follows the air gap region necessitates that the modeled locations of the right boundaries of these subsequent regions be increased by the same 0.00018 feet.

Due to an addition error, Calculation N-4080-002 (page 188) incorrectly modeled the right boundary coordinate of the Concrete Region at 4.23283 feet. The determination of the right

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boundary coordinate of the Concrete region is based on adding the thickness of the Concrete Region to the thicknesses of the Organic Paint, Carbon Steel and Air Gap Interface regions. The original calculations considered a Carbon Steel thickness of 0.02083 feet rather than the correct thickness of 0.66667 feet. Correcting this error, and adjusting for the change in the Air Gap Interface Region thickness, allows for the calculation of a 7th Region right boundary coordinate of 4.87885 feet:

Right Boundary Coordinate = 0.00075 ft + 0.66667 ft + 0.00035 ft + 4.21108 ftof Concrete Region = 4.87885 feet

The changes from the right boundary locations determined in Calculation N-4080-002 are:

1st Region: no change in the right boundary location 2nd Region: no change in the right boundary location

3rd Region: right boundary shifted from 0.66759 to 0.66777 feet 4th Region: right boundary shifted from 0.70926 to 0.70944 feet 5th Region: right boundary shifted from 0.7926 to 0.79278 feet 6th Region: right boundary shifted from 1.4426 to 1.44278 feet 7th Region: right boundary shifted from 4.23283 to 4.87885 feet

The Card Series set defining Heat Sink 19 is entered in the input data file as.

```
* HS #19 - REACTOR BLDG CYLINDER #3: SECTIONS WITH STIFFENERS &LIST POOL=119001, 100, 7, 0, 0, 0, 0, 1590.68/
&LIST POOL=119101, 5, 0.00075, 20, 0.66742, 3, 0.66777, 15, 0.70944, 20, 0.79278, 16, 1.44278, 20, 4.87885/
&LIST POOL=119201, 4, 1, 5, 2, 2, 2, 2/
&LIST POOL=119300, 0, 0/
&LIST POOL=119400, 9, 2, 1, 1/
```

As discussed in Design Input 4.8, the heat transfer coefficient control for the left boundary condition (adjacent to the organic paint) is modeled as the Uchida value. This is a condensing steam value dependent on the ratio of water vapor to air used in MSLB analyses. Therefore Item 2 in Card Series 119400 is 9.

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8.1.27.20 HS #20 - Vent Tunnels

The characteristics of the Vent Tunnels are as determined in Calculation N-4080-002 (Reference 6.1.g, pages 190 through 192) for Heat Sink 20.

Heat Sink #20 describes the Vent Tunnels as modeled:

Geometry Slab

Surface Area 2827 ft²

Organic Paint (material 4) thickness-Left 0.0005 ft (= 0.006 in)

Boundary

Carbon Steel (material 1) thickness-Right 0.03125 ft (= 0.375 in)

Boundary

Left Boundary condition Exposed to containment atmosphere

Right Boundary condition Insulated (approximating an infinitely thick tunnel wall)

Because there is no heat transfer across the right boundary, the bulk temperature control for the right boundary condition is not used by the COPATTA Code. Therefore, in this analysis the bulk temperature control for the right boundary condition is modeled as the containment vapor temperature for convective heat transfer or the saturation temperature at the containment steam partial pressure for condensing heat transfer (i.e., Option 2 for Item 5 of Card Series 1XX400). This differs from the modeling of Calculation N-4080-002, which employed Option 0 for Item 5 of Card Series 1XX400. Since the bulk temperature control for the right boundary condition has no meaning for this Heat Sink, the decision to model Item 5 with Option 2 rather than Option 0 has the beneficial consequence of allowing the use of any positive value to be modeled as the variable TCONT in Item 7 of Card Series 2.

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The Card Series set defining Heat Sink 20 is entered in the input data file as:

```
* HS #20 - VENT TUNNELS
&LIST POOL=120001, 23, 2, 0, 0, 0, 0, 2827/
&LIST POOL=120101, 10, 0.0005, 12, 0.03175/
&LIST POOL=120201, 4, 1/
&LIST POOL=120300, 0, 0/
&LIST POOL=120400, 9, 2, 0, 2/
```

As discussed in Design Input 4.8, the heat transfer coefficient control for the left boundary condition (adjacent to the organic paint) is modeled as the Uchida value. This is a condensing steam value dependent on the ratio of water vapor to air used in MSLB analyses. Therefore Item 2 in Card Series 120400 is 9.

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8.1.28 CARD SERIES 410001: Table 15

Card Series 410001 is a table that is used to describe the material properties in the heat sink calculations. The Card Series 410001 table includes the following data entered in columnar form:

- 1. thermal conductivity (BTU/hr-ft-°F)
- 2. volumetric heat capacity (BTU/ft3-oF)

The entries in Card Series 410001 define five materials. These materials include:

ITEMS 2 and 3: Material 1 - Carbon Steel

Material 1 is defined as Carbon Steel. Per Design Input Item 4.14.a, the thermal conductivity and volumetric heat capacity of Carbon Steel are:

$$k = 25 BTU/hr-ft-°F$$

 $\rho C_p = 54 BTU/ft^3-°F$

ITEMS 4 and 5: Material 2 - Concrete

Material 2 is defined as Concrete. Per Design Input Item 4.14.b, the thermal conductivity and volumetric heat capacity of Concrete are:

$$k = 0.8 \text{ BTU/hr-ft-}^{\circ}\text{F}$$

 $\rho C_o = 30 \text{ BTU/ft}^{3}\text{-}^{\circ}\text{F}$

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Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

Sheet No. 127

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
0	S. Oliver	12/30/93	J. Elliott	1/4/94				THE RESERVE OF THE PARTY OF THE	THE SHOW COMMO	EV
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ITEMS 6 and 7: Material 3 - Stainless Steel

Material 3 is defined as Stainless Steel. Per Design Input Item 4.14.c, the thermal conductivity and volumetric heat capacity of Stainless Steel are:

$$k = 10 BTU/hr-ft-°F$$

 $\rho C_p = 54 BTU/ft^3-°F$

ITEMS 8 and 9: Material 4 - Organic Paint Coating

Material 4 is defined as Organic Paint Coating. Per Design Input Item 4.14.d, the thermal conductivity and volumetric heat capacity of Organic Paint Coating are:

$$k = 0.1 BTU/hr-ft-°F$$

 $\rho C_p = 20 BTU/ft^3-°F$

ITEMS 10 and 11: Material 5 - Air Gap (@ 200 °F)

Material 5 is defined as the Air Gap Interface between the Containment Building walls and the Carbon Steel Liner, at a containment air temperature of 200 °F. Per Design Input Item 4.14.e, the thermal conductivity and volumetric heat capacity of the Air Gap are:

$$k = 0.0174 \text{ BTU/hr-ft-}^{\circ}\text{F}$$

 $\rho C_p = 0.0103 \text{ BTU/ft}^{3} ^{\circ}\text{F}$

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Sheet No. 128

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
0	S. Oliver	12/30/93	J. Elliott	1/4/94				M. M. C.		EV
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8.1.29 CARD SERIES 420001: Table 16

Card Series 420001 is used to specify arbitrary constant non-condensing heat transfer coefficients to be assumed at any heat sink surface. This table is required if a heat transfer coefficient control of 10 to 15 is specified for Items 2 or 4 in Card Series 1XX400. In this model, heat transfer coefficient controls other than 10 to 15 are specified for Items 2 and 4 in Card Series 1XX400. Therefore, this Card Series is not used.

8.1.30 CARD SERIES 430001: Table 17

Card Series 430001 is used to describe the time-dependent condensing heat transfer coefficients to be assumed at any heat sink surface. This table is required if a heat transfer coefficient control of 5 or 8 is specified for Items 2 or 4 in Card Series 1XX400. In this model, heat transfer coefficient controls other than 5 or 8 are specified for Items 2 and 4 in Card Series 1XX400. Therefore, this Card Series is not used.

8.1.31 CARD SERIES 440001: Table 18

Card Series 430001 is used to describe an additional set of time-dependent condensing heat transfer coefficients to be assumed at any heat sink surface. This table is required if a heat transfer coefficient control of 6 is specified for Items 2 or 4 in Card Series 1XX400. In this model, heat transfer coefficient controls other than 6 are specified for Items 2 and 4 in Card Series 1XX400. Therefore, this Card Series is not used.

8.1.32 CARD SERIES 450001: Table 19

Card Series 450001 is used to describe the temperature-dependent non-condensing heat transfer coefficients to be assumed at any heat sink surface. This table is required if a heat transfer coefficient control of 7 is specified for Items 2 or 4 in Card Series 1XX400. In this model, heat transfer coefficient controls other than 7 are specified for Items 2 and 4 in Card Series 1XX400. Therefore, this Card Series is not used.

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REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
0	S. Oliver	12/30/93	J. Elliott	1/4/94		THE RESERVE OF THE PARTY OF THE		THE STREET PRINTED PRINTED AND THE STREET, MADE AND		E
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8.1.33 CARD SERIES 500000: End Card

If heat sink data is used, this card must follow the complete set of base case data. Otherwise it may be omitted. In this calculation, heat sink data is used. The card contains the following fixed information in Columns 2 through 19:

&LIST POOL=500000/

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Project or DCP/MMP SONGS Units 2 & 3 Calc. No. N-4080-027

*MSLB CASE, 102% POWER, LOSS OF ONE COOLING TRAIN, OFFSITE POWER AVAIL.

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Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

Sheet No. 130

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
0	S. Oliver	12/30/93	J. Elliott	1/4/94						E
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9 COPATTA INPUT FILES

INPUT FILE NAME: MSLB N01.DAT

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&LIST POOL=0,0,1,0,1,0,0,0,0/
&LIST POOL=1, 1E4, 16.2, 2.305E6, 120, 0.6, 20, 582.945, 1, 1, 0, 14.7, 0.5/
&LIST POOL=2, 0,0,0,0,0,120,2E7/
&LIST POOL=3,0,0,0,0,0,2E7,0,0,0,0,0
&LIST POOL=4,0,0,0,0,0,0,0,0,0,0,0,0,0,0,0,0,0
&LIST POOL=5,2,15,1E4,0,0,0,105/
&LIST POOL=6,0,0,0/
&LEAK NOPEN=0/
&LIST POOL=101,
         0,
       2E7,
                 0/
&LIST POOL=201,
         0,
                 0,
       2E7,
                 0/
&LIST POOL=301,
                  0.
                         5.145520E7,
                                       1.195589E3,
                0.22,
                        4.869032E7,
                                        1.197482E3,
                0.42,
                                        1.198466E3,
                        4.622234E7,
                0.62,
                         4.405936E7,
                                        1.199410E3,
                1.08,
                        4.003276E7,
                                        1.201595E3,
                        3.688855E7,
                1.58,
                                         1.201757E3,
                2.08,
                        3.445970E7,
                                        1.202018E3,
                2.58,
                        3.326288E7,
3.152606E7,
                                        1.200986E3,
                3.58,
                                         1.201058E3,
                4.58,
                                        1.201655E3
                        3.028468E7.
                5.58,
                       2.940080E7,
                                       1.201123E3,
                       2.874870E7,
                6.58,
                                        1.201126E3
                7.58,
                        2.706574E7
                                        1.204404E3,
                8.58,
                                        1.204367E3,
                        2.468326E7,
                9.58,
                        2.294968E7,
                                        1.204238E3,
                         2.160122E7,
                                        1.203908E3,
               10.58,
                                        1.203195E3,
               12.58,
                        1.943143E7,
               14.58,
                         1.765940E7,
                                        1,202277E3,
               16.58,
                         1.637240E7,
                                         1.201556E3.
               18.58,
                        1.544720E7.
                                        1.200963E3,
               20.58,
                        1.473293E7,
                                        1.200422E3,
                        1.327525E7,
               25.58,
                                        1.198820E3,
              30.58,
                         1.221858E7,
                                         1.197825E3,
              35.58,
                        1.146406E7,
                                        1.196753E3,
                         1.059131E7,
               40.58,
                                        1.195307E3,
                        9.801216E6,
               45.58,
                                         1.194165E3
               50.58,
                        9.132588E6,
                                        1.193086E3
              60.58,
                        8.280324E6,
                                        1.190935E3,
                         7.245576E6,
               61.08,
                                       1.190949E3
                         5.803344E6,
              62.08.
                                         1.189165E3,
                                        1.184658E3,
               62.58,
                         3.238704E6,
                         3.948840E5,
               64.58,
                                        1.179953E3,
              68.58,
                         1.074240E5,
                                         1.251072E3,
               71.08,
                                  0,
                2E7,
                                  0,
                                                   0/
&LIST POOL=401,
         0.
       2E7,
                0,
                        0/
&LIST POOL=501,
                0,
         0,
                        0,
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	2E7,	0, 0/								
	&LIST POOL=60	0. 0.								ı
	&LIST POOL=70	0, 0/								l
	0,	0, 0,	0,							No.
	2E7, &LIST POOL=80	1,	0/							l
	50,	0, 0,	0, 100, 1	00,						l
	50, 8. 2E7, 8.	02E5, 0,	0, 100, 1	00,						l
	&LIST POOL=90	1,	0, 100, 1	007						
	0, 2E7,	0, 0/								
	&LIST POOL=10	01, 100, 2.0,								l
	24, &LIST POOL=11	100, 2.0/								
	10	5, 0, 0, 1.670E6,								
	12 13	0, 1.670E6, 0, 3.020E6,								l
	14	0, 4.570E6, 0, 6.320E6,								THE REAL PROPERTY.
	16	O, 8.270E6,								-
	18	0, 1.040E7, 0, 1.273E7,								
		0, 1.523E7, 0, 1.788E7,								ı
	21	0, 2.068E7, 0, 2.361E7,								ı
	23	0, 2.664E7,								
	25	0, 2.974E7, 0, 3.291E7,								
		0, 3.611E7, 0, 3.931E7,								
	28	0, 4.252E7,								I
	29	7, 4.474E7, 0, 4.569E7,								I
	&LIST POOL=12	0, 4.882E7/								
		0, 0.729, 1, 0.737,								ı
	0.	2, 0.747,								l
	0.	3, 0.757, 4, 0.771,								
	0.	5, 0.738, 6, 0.809,								I
	0.	7, 0.832, 8, 0.863,								-
	0.	9, 0.912,								I
	1.	0, 0.961, 1, 0.983,								I
		2, 0.995, 3, 1.000/								ı
	&LIST POOL=90	01, 5, 0.05,	0.1, 50,							-
		10, 0.05,	0.25, 20,							
		15, 0.05, 20, 0.05,	0.50, 10, 0.50, 10,							ESCONSES.
		100, 0.1,	1.0, 10, 5.0, 10,							-
		220, 110,	2.01							-

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	&LIST POOL=99 * HS #1 - REAC &LIST POOL=10 &LIST POOL=10 &LIST POOL=10	700, 2.0, 2E3, 5.0, 1E4, 50.0, 1E5, 250, 1E6, 500, 1E7, 500, 2E7, 500, 99/ TOR BUILDING (1001, 100, 7, 1101, 5, 0.00(3, 0.02) 20, 0.23(21, 4.06) 1201, 4, 1, 5 1300, 0, 0/	0, 0, 0, 0, 34 075, 3, 0.0 193, 10, 0.0 028, 37, 1.0 363/ , 2, 2, 2, 2/	2158, 6360,						INSTANCES STREET, PRINCIPAL AND
	&LIST POOL=10 * HS #2 - CYLI &LIST POOL=10 &LIST POOL=10 &LIST POOL=10 &LIST POOL=10	1400, 9, 2, 1 NDER WALL BETY 2001, 100, 7, 2101, 5, 0.000 3, 0.02 20, 0.146 21, 4.35 2201, 4, 1, 5 2300, 0, 0/	WEEN EL. 29'6" 0, 0, 0, 0, 38 075, 3, 0.0 193, 10, 0.0 694, 37, 0.91 526/ , 2, 2, 2, 2/	120/ 2158, 6360,						CONTRACTOR (CANADASSICATION) PROSESSIONAL PROPERTY (CANADASSICATION)
	&LIST POOL=10 &LIST POOL=10	NDER WALL BETW 3001, 100, 7, 3101, 5, 0.000 3, 0.02 20, 0.140 21, 4.35	0, 0, 0, 0, 66 075, 3, 0.0 193, 10, 0.0 694, 37, 0.91	67.38/ 2158, 6360,						CANADA STATE OF THE SECOND SEC
	&LIST POOL=10	3300, 0, 0/ 3400, 9, 2, 0, MAT (OTHER TH) 4001, 53, 5, 0 4101, 3, 0.00	, 2/ AN REACTOR BASE 0, 0, 0, 0, 128 0067, 7, 2698, 2, 1.54	00/						WATCHWELLING CONTRACTOR BY LOWING BY
	&LIST POOL=10	4201, 4, 2, 2, 4300, 0, 0/ 4400, 3, 3, 0, TOR BASEMAT & 5001, 70, 4, 0	, 1, 2/ , 3/ s.g. PEDESTALS 0, 0, 0, 0, 164 158, 10,	4/ 0.1,						MANAGEMENT CONTRACTOR AND ADDRESS OF THE PARTY.
	&LIST POOL=10	5201, 4, 2, 2, 5300, 0, 0, 5400, 3, 3, 0, TOR CAVITY WAI 6001, 93, 5, 6101, 5, 11.75	, 2/ , 3/ LLS BELOW EL. 1 1, 11.75, 0, 0, 5192, 7, 11. 9923, 30, 19.	5/0" 21.5/ 77292,						Print Street Str
	&LIST POOL=10 &LIST POOL=10 &LIST POOL=10 * HS #7 - REAC	6300, 0, 0/ 6400, 3, 3, 0,	, 2, 2/							Section Committee Committee

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	er 12/30/93	J. Elliott	1/4/94		NA AREA CONTROL OF THE PERSON NAMED IN CONTROL OF THE PERSON N			DATE	E
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&LIST POOL	15, 0.46 20, 4.00 20, 4.00 20, 4.00 20, 4.00 20, 4.00 20, 4.00 20, 4.00 20, 20 20, 20 20 20, 20 20 20 20 20 20 20 20 20 20 20 20 20 2	J. Elliott 0192, 20, 2.0 0192/ 2, 2, 2/ 0, 2/ CANAL WALLS 0, 0, 0, 0, 9200 1563, 20, 2 1563, 5, 4.01 2, 2, 4/ 9, 2/ LLS, UNLINED REFL 0, 0, 0, 0, 4197 0, 0, 0, 0, 1747 00, 1, 50, 1.71 2, 2/ 0, 2/ HER THAN BASEMATS 0, 0, 0, 0, 1747 0014, 5, 0.005348 05348, 15, 0.5053 05348, 3, 1.50601 2, 2, 4/ 9, 2/ (EXCEPT STAINLES 0, 0, 0, 0, 5728 0, 0, 0, 0, 5728 0, 0, 0, 0, 5728 0, 0, 0, 0, 5728 0, 2/ ARBON STEEL - THI 0, 0, 0, 0, 0, 516/ 005, 17, 0.084, 0, 25, 0.310849/ 1, 1/ 0, 2/ RRBON STEEL: 1.00	1/4/94 1/4/94 100, /0	INT WAL		DATE	IRE	DATE	٧

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Project or DCP/MMP_SONGS Units 2 & 3 Calc. No. N-4080-027

&L1ST POOL=500000/

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&LIST POOL=116201, 1/
&LIST POOL=116300, 0, 0/
&LIST POOL=116400, 9, 2, 0, 2/
* HS #17 - MISCELLANEOUS STAINLESS STEEL
 &LIST POOL=117001, 16, 1, 0, 0, 0, 0, 24048/
&LIST POOL=117101, 15, 0.01747/
&LIST POOL=117201, 3/
 &LIST POOL=117300, 0, 0/
 &LIST POOL=117400, 9, 2, 0, 2/
* HS #18 - UNLINED REFUELING CANAL WALLS BELOW EL. 63'6"
 &LIST POOL=118001, 48, 4, 0, 0, 0, 0, 3700/
&LIST POOL=118101, 5, 0.00192, 7, 0.02292,
15, 0.40192, 20, 2.00192/
 &LIST POOL=118201, 4, 2, 2, 2/
 &LIST POOL=118300, 0, 0/
&LIST POOL=118400, 9, 2, 0, 2/
* HS #19 - REACTOR BLDG CYLINDER #3: SECTIONS WITH STIFFENERS
 &LIST POOL=119001, 100, 7, 0, 0, 0, 0, 1590.68/

&LIST POOL=119101, 5, 0.00075, 20, 0.66742, 3, 0.66777,

15, 0.70944, 20, 0.79278, 16, 1.44278,
                              20, 4.87885/
&LIST POOL=119201, 4, 1, 5, 2, 2, 2, 2/
&LIST POOL=119300, 0, 0/
&LIST POOL=119400, 9, 2, 1, 1/
* HS #20 - VENT TUNNELS
 &LIST POOL=120001, 23, 2, 0, 0, 0, 0, 2827/
&LIST POOL=120101, 10, 0.0005, 12, 0.03175/
 &LIST POOL=120201, 4, 1/
 &LIST POOL=120300, 0, 0/
&LIST POOL=120400, 9, 2, 0, 2/
 &LIST POOL=410001,
                                54.
                  25,
                  0.8,
                                30,
                   10,
                                54,
            0.1, 20, 0.0174, 0.0103/
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REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
0	S. Oliver	12/30/93	J. Elliott	1/4/94						E
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10 SELECTED OUTPUT DATA

The tabulated data presented in Sections 10.1 and 10.2 consists of partial output of the COPATTA code. This data is then used as the input to the plots in Section 2.

All values are taken directly from output files produced by the COPLOTTA (Ref. 6.5.a pg. E-3) program in conjunction with the COPATTA output file except the gauge pressure with respect to the outside atmosphere (psig w/r 14.7 psia). The COPATTA output file assumes that the initial containment pressure is the reference pressure for determining gauge pressure. Because this analysis is concerned with the pressure differential across the containment structure, 1.5 psi is added to the gauge pressure presented in the COPATTA output (psig w/r 16.2 psia).

10.1

TIME (SECONDS)	SUMP TEMP (DEG-F)	VAPOR TEMP (DEG-F)	TOTAL PRESSURE (PSIA)	GAUGE PRESSURE PSIG (W/R 14.7 psia)	LEFT BOUNDARY TEMPERATURE HS#1 (DEG-F)	UCHIDA CONDENSING HTC (BTU/FT2-F-HR)
0.05	-1.0e-07	123.329	16.4013	1.701269	118.3676	7.65926
0.1	-1.0e-07	126.654	16.6006	1.900648	118.3676	8.07424
0.2	-1.0e-07	133.06	16.992	2.291994	118.3676	9.24911
0.3	-1.0e-07	139.155	17.3734	2.67341	118.3676	9.77065
0.4	122.262	144.967	17.7452	3.0452	118.3676	10.6752
0.5	125.256	150.503	18.1074	3.40736	118.3676	11.9305
0.6	127.832	155.788	18.4607	3.7607	118.3676	12.9467
0.7	130.22	160.842	18.8057	4.10575	118.3676	13.7865
0.8	132.398	165.692	19.1436	4.44364	118.3676	14.4938
0.9	134.492	170.35	19.4745	4.77447	118.3676	15.0974
1	136.438	174.822	19.7982	5.09819	118.3676	15.6182
1.1	138.237	179.119	20.1149	5.41489	118.3676	16.0718
1.2	139.949	183.255	20.4256	5.72557	118.3676	16.4719
1.3	141.605	187.241	20.7308	6.03076	118.3676	16.8278
1.4	143.226	191.085	21.0305	6.33054	118.3676	17.2929
1.5	144.784	194.791	21.3248	6.62481	118.3676	17.8663
1.6	146.264	198.365	21.6137	6.9137	118.3676	18.3849
1.7	147.686	201.823	21.898	7.19796	118.3676	18.8571
1.8	149.062	205.173	22.178	7.47799	118.3676	19.2894
1.9	150.401	208.42	22.4539	7.75388	118,3676	19.6864

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ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
S. Oliver	12/30/93	J. Elliott	1/4/94	The state of the s	THE SHARE A SECURITARISM STATE OF SHARE SH	COMMON CO	NAMES OF PERSONS ASSESSED.		E
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TIME (SECONDS)	SUMP TEM! (DEG-F)	VAPOR TEMP (DEG-F)	TOTAL PRESSURE (PSIA)	GAUGE PRESSURE PSIG (W/R 14.7 psia)	LEFT BOUNDARY TEMPERATURE HS#1 (DEG-F)	UCHIDA CONDENSING HTC (BTU/FT2-F-HR)
2	151.692	211.566	22.7255	8.0255	118.3676	20.0522
2.1	152.926	214.616	22.9929	8.29293	118.3676	20.3903
2.2	154.115	217.583	23.2574	8.55742	118.3676	20.7051
2.3	155.266	220.475	23.5195	8.81948	118.3676	20.9996
2.4	156.392	223.296	23.7793	9.07927	118.3676	21.4134
2.5	157.493	226.045	24.0365	9.33651	118.3676	21.8023
2.6	158.553	228.725	24.2913	9.59132	118.3676	22.1681
2.7	159.576	231.346	24.5442	9.84423	118.3676	22.5134
2.8	160.569	273.913	24.7955	10.09545	118.3676	22.8399
2.9	161.536	236.428	25.0452	10.34519	118.3676	23.1493
3	162.479	238.89	25.2931	10.59308	118.3676	23.4427
3.1	163.402	241.302	25.5393	10.8393	118.3676	23.7214
3.2	164.307	243.665	25.7839	11.08386	118.3676	23.9864
3.3	165.201	245.984	26.027	11.32699	118.3676	24.3979
3.4	166.086	248.254	26.2682	11.5682	118.3676	24.7988
3.5	166.963	250.48	26.5078	11.8078	118.3676	25.1812
3.6	167.828	252.661	26.7458	12.0458	118.3676	25.5464
3.7	168.671	254.802	26.9824	12.2824	118.3676	25.896
3.8	169.494	256.909	27.218	12.518	118.3676	26.231
3.9	170.3	258.978	27.4522	12.7522	118.3676	26.5524
4	171.09	261.011	27.6852	12,9852	118.3676	26.861
4.1	171.866	263.009	27.917	13.217	118.3676	27.1575
4.2	172.629	264.976	28.1479	13, 4479	118.3676	27.4426
4.3	173.379	266.908	28.3773	13.6.73	118.3676	27.717
4.4	174.119	268.809	28.6056	13.9056	118.3676	27.9811
4.5	174.848	270.678	28.8328	14.1328	118.3676	28.2357
4.6	175.568	272.516	29.0587	14.3587	118.3676	28.4811
4.7	176.279	274.324	29.284	14.584	118.3676	28.7182
4.8	176.976	276.106	29.5081	14.8081	118.3676	28.9472
4.9	177.661	277.857	29.7311	15.0311	118.3676	29.3858
5	178.34	279.58	29.9531	15.2531	134.467	29.8756
5.25	180.003	283.769	30.5038	15.8038	134.467	31.0332
5.5	181.623	287.798	31.0489	16.3489	134.467	32.1034
5.75	183.202	291.673	31.5878	16.8878	134.467	33.0962

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Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
0	S. Oliver	12/30/93	J. Elliott	1/4/94				ACCORDANGED AND ACCOUNTS OF THE PARTY OF THE		E
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TIME (SECONDS)	SUMP TEMP (DEG-F)	VAPOR TEMP (DEC·F)	TOTAL PRESSURE (PSIA)	GAUGE PRESSURE PSIG (W/R 14.7 psia)	LEFT BOUNDARY TEMPERATURE HS#1 (DEG-F)	UCHIDA CONDENSING HTG (BTU/FT2-F-HR
6	184.731	295.414	32.122	17.422	134.467	34.021
6.25	186.201	299.03	32.6522	17.9522	134.467	34.8847
6.5	187.622	302.522	33.1773	18.4773	134.467	35.6932
6.75	188.998	305.897	33.6972	18.9972	134.467	36.4499
7	190.336	309.168	34.21	19.51	134.467	37.2438
7.25	191.646	312.33	34.7142	20.0142	134.467	38.2796
7.5	192.93	315.39	35.2103	20.5103	134.467	39.2477
7.75	194.18	318.343	35.6973	20.9973	134.467	40.1527
8	195.385	321.166	36.1733	21.4733	134.467	40.9962
8.25	196.547	323.85	36.6356	21.9356	134.467	41.7833
8.5	197.67	326.407	37.0853	22.3853	134.467	42.5188
8.75	198.755	328.852	37.5235	22.8235	134.467	43.2081
9	199.806	331.198	37.9523	23.2523	134.467	43.8581
9.25	200.825	333.449	38.372	23.672	134.467	44.472
9.5	201.814	335.613	38.7825	24.0825	134.467	45.0522
9.75	202.774	337.701	39.1862	24.4862	134.467	45.6019
10	203.707	339.706	39.5807	24.8807	150.5152	46.2353
10.5	205.52	343.504	40.3475	25.6475	150.5152	48.0698
11	207.262	347.04	41.0863	26.3853	150.5152	49.7396
11.5	208.921	350.35	41.801	27.101	150.5152	51.2703
12	210.489	353.461	42.4941	27.7941	150.5152	52.6774
12.5	211.974	356.364	43.1615	28.4615	150.5152	53.9735
13	213.384	359.092	43.8071	29.1071	150.5152	55.1722
13.5	214.727	361.661	44.4333	29.7333	150.5152	56.2865
14	216.01	364.082	45.0402	30.3402	150.5152	57.3242
14.5	217.239	366.377	45.6307	30.9307	150.5152	58.2917
15	218.421	368.534	46.2014	31.5014	163.8227	59.1971
15.5	219.584	370.57	46.7556	32.0555	163.8227	60.047
16	220.695	372.501	47.2956	32.5956	163.8227	60.8486
16.5	221.754	374.34	47.8222	33.1222	163.8227	61.6054
17	222.766	376.092	48.3384	33.6384	163.8227	62.3222
17.5	223.738	377.784	48.8431	34.1431	163.8227	63.0092
18	224.675	379.393	49.3369	34.6369	163.8227	64.3464
18.5	225.583	380.932	49.8201	35.1201	163.3227	65.6197

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REV	ORIGINATOR	DATE	!RE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
0	S. Oliver	12/30/93	J. Elliott	1/4/94						E
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TIME (SECONDS)	SUMP TEMP (DEG-F)	VAPOR TEMP (DEG-F)	PRESSURE (PSIA)	GAUGE PRESSURE PSIG (W/R 14.7 psia)	LEFT BOUNDARY TEMPERATURE HS#1 (DEG-F)	UCHIDA CONDENSING HTC (BTU/FT2-F-HR)
19	226.464	382.404	50.2934	35.5934	163.8227	66.8348
19.5	227.319	383.825	50.7586	36.0586	163.8227	67.998
20	228.15	385.179	51.2148	36.5148	174.6759	69.1125
21	229.748	387.75	52.1043	37.4043	174.6759	71.2276
22	231.255	390.142	52.9661	38.2661	174.6759	73.1655
23	232.673	392.223	53.7636	39.0636	174.6759	74.9654
24	234.009	394.292	54.5721	39.8721	174.6759	76.6404
25	235.276	396.219	55.3554	40.6554	174.6759	78.2016
26	236.482	398.013	56.1143	41.4143	174.6759	79.66
27	237.633	399.702	56.854	42.154	174.6759	81.0319
28	238.735	401.29	57.5755	42.8755	174.6759	82.3258
29	239.787	402.783	58.2793	43.5793	174.6759	83.5478
30	240.788	404.195	58.9661	44.2661	192.9141	84.7033
31	241.744	405.527	59.6363	44.9363	192.9141	85.7976
32	242.662	406.791	60.2935	45.5935	192.9141	86.84
33	243.545	407.992	60.9383	46.2383	192.9141	87.8346
34	244.397	409.133	61.571	46.871	192.9141	88.7846
35	245.219	410.217	62.1917	47.4917	192.9141	89.6925
36	246.015	411.248	62.8005	48.1005	192.9141	90.5605
37	246.784	412.224	63.3963	48.6963	192.9141	91.3895
38	247.525	413.15	63.979	49.279	192.9141	92.1814
39	248.24	414.021	64.5484	49.8484	192.9141	92.9385
40	248.932	414.84	65.1046	50.4046	206.8357	93.6625
41	249.601	415.617	65.6484	50.9484	206.8357	94.3554
42	250.249	416.352	66.1804	51.4804	206.8357	95.0197
43	250.876	417.052	66.7013	52.0013	206.8357	95.657
44	251.484	417.717	67.211	52.511	206.8357	96.2688
45	252.075	418.348	67.7096	53.0096	206.8357	96.8561
46	252.65	418.943	68.197	53.497	206.8357	97.4203
47	253.21	419.506	68.6747	53.9747	206.8357	97.9638
48	253.756	420.041	69.1428	54.4428	206.8357	98.9752
49	254.29	420.545	69.6009	54.9009	206.8357	99.9845
50	254.811	421.024	70.0495	55.3495	218.549	100.957
51	255.321	419.305	70.3583	55.6583	218,549	102.008

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REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
0	S. Oliver	12/30/93	J. Elliott	1/4/94	A STATE PART LINE WELL	A MANAGEMENT OF THE PARTY AND		Principle and edicate community and all community and		E
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TIME (SECONDS)	SUMP TEMP (DEG-F)	VAPOR TEMP (DEG-F)	TOTAL PRESSURE (PSIA)	GAUGE PRESSURE PSIG (W/R 14.7 psia)	LEFT BOUNDARY TEMPERATURE HS#1 (DEG-F)	UCHIDA CONDENSING HTG (BTU/FT2-F-HR)
52	255.816	417.525	70.6546	55.9546	218.549	103.028
53	256.299	415.765	70.9459	56.2459	218.549	104.018
54	256.77	414.02	71.2315	56.5315	218.549	104.979
55	257.229	412.293	71.512	56.812	218.549	105.913
56	257.677	410.587	71.7876	57.0876	218.549	106.821
57	258.115	408.899	72.0584	57.3584	218.549	107.703
58	258.541	407.227	72.324	57.624	218.549	108.561
59	258.958	405.56€	72.5841	57.8841	218.549	109.395
60	259.366	403.929	72.8397	58.1397	228.8108	110.206
61	259.762	402.283	73.0781	58.3781	228.8108	110.976
62	260.147	400.462	73.2126	58.5126	228.8108	111.562
63	260.517	398.286	73.1564	58.4564	228.8108	111.831
64	260.867	395.859	72.9588	58.2588	228.8108	111.866
65	261.197	393.296	72.6742	57.9742	228.8108	111.752
66	261.507	390.724	72.3741	57.6741	228.8108	111.607
67	261.798	388.16	72.073	57.373	228.8108	111.458
68	262.07	385.597	71.7707	57.0707	228.8108	111.305
69	262.325	383.012	71.4651	56.7651	228.8108	111.149
70	262.564	380.356	71.1533	56.4533	233.5631	110.991
71	262.789	377.713	70.8425	56.1425	233.5631	110.831
72	263	375.124	70.5376	55.8376	233.5631	110.672
73	263.198	372.544	70.2358	55.5358	233.5631	110.517
74	263.384	369.976	69.9371	55.2371	233.5631	110.365
75	263.559	367.413	69.6411	54.9411	233.5631	110.216
76	263.724	364.856	69.3478	54.6478	233.5631	110.071
77	263.879	362.311	69.0578	54.3578	233.5631	109.929
78	264.025	359.771	68.7701	54.0701	233.5631	109.79
79	264.162	357.242	68.4852	53.7852	233.5631	109.654
80	264.292	354.72	68.2029	53.5029	235.9147	109.521
81	264.413	352.21	67.9234	53.2234	235.9147	109.391
82	264.528	349.706	67.6465	52.9465	235.9147	109.265
83	264.636	347.211	67.3717	52.6717	235.9147	109.141
84	264.737	344.724	67.0994	52.3994	235.9147	109.019
85	264.833	342.246	66.8296	52.1296	235.9147	108.901

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REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	F
0 S	S. Oliver	12/30/93	J. Elliott	1/4/94				A MAN AND AND AND AND AND AND AND AND AND A		E
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TIME (SECONDS)	SUMP TEMP (DEG-F)	VAPOR TEMP (DEG-F)	TOTAL PRESSURE (PSIA)	GAUGE PRESSURE PSIG (W/R 14.7 psia)	LEFT BOUNDARY TEMPERATURE HS#1 (DEG-F)	UCHIDA CONDENSING HT (BTU/FT2-F-HR
86	264.923	339.777	66.5621	51.8621	235.9147	108.785
87.00001	265.007	337.316	66.2969	51.5969	235.9147	108.673
88	265.087	335.017	66.0851	51.3851	235.9147	108.562
89	265.163	332.568	65.8237	51.1237	235.9147	108.454
90	265.233	330.128	65.5644	50.8644	237.6333	108.349
91	265.3	327.691	65.3068	50.6068	237.6333	108.246
92.00001	265.363	325.265	65.0516	50.3516	237.6333	108.145
93	265.421	322.843	64.798	50.0979	237.6333	108.047
94	265.476	320.427	64.5461	49.8461	237.6333	107.952
95	265.527	317.979	64.2839	49.5839	237.6333	107.858
96	265.575	315.577	64.0356	49.3356	237.6333	107.768
97	265.619	313.185	63.7894	49.0894	237.6333	107.679
98	265.661	310.795	63.5444	48.8444	237.6333	107.593
99	265.699	308.417	63.3017	48.6017	237.6333	107.508
100	265.735	306.025	63.0538	48.3538	238.7824	107.426
105	265.872	294.822	61.9142	47.2142	238.7824	107.194
110	265.958	283.128	60.7529	46.0529	238.7824	106.856
115	266.003	272.393	59.6665	44.9665	238.7824	106.563
120	266.032	267.123	58.9567	44.2567	238.7824	105.696
125	266.034	266.562	58.5725	43.8725	238.7824	104.797
130	266.013	266.019	58.2038	43.5038	238.7824	103.92
135	265.973	265.493	57.8489	43.1489	238.7824	103.06
140	265.917	264.982	57.5066	42.8066	238.7824	102.217
145	265.849	264.485	57.176	42.476	238.7824	101.391
150	265.769	264	56.8555	42.1555	241.4326	100.588
155	265.679	263.527	56.5446	41.8446	241.4326	99.7883
160	265.584	263.23	56.3501	41.6501	241.4326	99.0251
165	265.484	262.777	56.0557	41.3557	241.4326	98.204
170	265.377	262.333	55.7685	41.0685	241.4326	97.7185
175	265.265	261.898	55.4887	40.7887	241.4326	97.343
180	265.149	261.472	55.216	40.516	241.4326	96.9662
185	265.029	261.054	54.95	40.25	241.4326	96.5938
190	264.905	260.643	54.6903	39.9903	241.4326	96.2254
195	264.779	260.241	54.4369	39.7369	241.4326	95.861

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REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
0	S. Oliver	12/30/93	J. Elliott	1/4/94		ACCOUNT TO THE PERSON OF THE P				E
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TIME (SECONDS)	SUMP TEMP (DEG-F)	VAPOR TEMP (DEG-F)	TOTAL PRESSURE (PSIA)	GAUGE PRESSURE PSIG (W/R 14.7 psia)	LEFT BOUNDARY TEMPERATURE HS#1 (DEG-F)	UCHIDA CONDENSING HTC (BTU/FT2-F-HR)
200	264.65	259.845	54.1893	39.4893	241.9631	95.5004
210	264.385	259.074	53.7106	39.0106	241.9631	94.7904
220	264.111	258.33	53.2533	38.5533	241.9631	94.0954
230	263.83	257,612	52.8157	38.1157	241.9631	93.4144
240	263.544	256.916	52.3963	37.6963	241.9631	92.7467
250	263.256	256.242	51.9936	37.2936	241.2001	92.0912
260	262.965	255.589	51.6063	36.9063	241.2001	91.4543
270	262.673	254.953	51.2332	36.5332	241.2001	90.822
280	262.389	254.502	50.9702	36.2702	241.2001	90.1887
290	262.098	253.897	50.6201	35.9201	241.2001	89.5724
300	261.806	253.308	50.2815	35.5815	240.0503	88.9708
310	261.512	252.733	49.9542	35.2542	240.0503	88.3715
320	261.217	252.172	49.6368	34.9368	240.0503	87.7787
330	260.922	251.623	49.3289	34.6289	240.0503	87.193
340	260.626	251.086	49.0297	34.3297	240.0503	86.6137
350	260.331	250.56	48.7389	34.0389	238.6837	86.0405
360	260.037	250.045	48.4561	33.7561	238.6837	85.4731
370	259.743	249.541	48.1812	33.4812	238.6837	84.9118
380	259.45	249.047	47.9138	33.2138	238.6837	84.3567
390	259.157	248.563	47.6533	32.9533	238.6837	83.807
400	258.863	248.087	47.3994	32.6994	237.136	83.2626
420	258.268	247.159	46.908	32.208	237.136	82.1913
440	257.666	246.256	46.4357	31.7357	237.136	81.1311
460	257.06	245.375	45.9809	31.2809	237.136	80.0729
480	256.455	244.684	45.6283	30.9283	237.136	79.0063
500	255.847	243.838	45.201	30.501	234.1299	77.9553
520	255.239	243.01	44.7876	30.0876	234.1299	76.9162
540	254.63	242.2	44.3875	29.6875	234.1299	75.8739
560	254.022	241.406	43.9996	29.2996	234.1299	74.8371
580	253.415	240.623	43.6215	28.9215	234.1299	73.7976
600	252.809	239.85	43.2525	28.5525	231.2043	72.7557
620	252.206	239.09	42.8929	28.1929	231.2043	71.7136
640	251.604	238.34	42.5425	27.8425	231.2043	70.6714
660	251.005	237.602	42.2007	27.5007	231.2043	69.6284

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0	S. Oliver	12/30/93	J. Elliott	1/4/94			-	Company of the Compan		EV
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TIME (SECONDS)	SUMP TEMP (DEG-F)	VAPOR TEMP (DEG-F)	TOTAL PRESSURE (PSIA)	GAUGE PRESSURE PSIG (W/R 14.7 psia)	LEFT BOUNDARY TEMPERATURE HS#1 (DEG-F)	UCHIDA CONDENSING HTG (BTU/FT2-F-HR
680	250.409	236.873	41.8671	27.1671	231.2043	68.5844
700	249.814	236.154	41.541	26.841	228.0915	67.5469
750.0001	248.347	234.391	40.7559	26.0559	226.5721	64.9502
800	246.923	232.846	40.0842	25.3842	225.1947	62.6494
850	245.539	231.16	39.3675	24.6675	223.8459	61.3454
900	244.191	229.51	38.6827	23.9827	222.5382	60.0193
950	242.876	227.893	38.0275	23.3275	221.2714	58.6769
1000	241.595	226.316	37.403	22.703	219.9015	57.3202
1050	240.35	224.778	36.8077	22.1077	218.5336	55.9533
1100	239.132	223.274	36.2384	21.5384	217.1893	54.5785
1150	237.943	221.801	35.693	20.993	215.8755	53.1855
1200	236.788	220.694	35.2359	20.5359	214.6037	51.8467
1250	235.657	219.11	34.7265	20.0265	213.426	50.328
1300	234.555	217.706	34.2373	19.5373	212.2342	48.8724
1350	233.479	216.325	33.7663	19.0663	211.0605	47.402
1400	232.427	214.967	33.3123	18.6123	209.9121	45.9508
1450	231.396	213.624	32.8725	18.1725	208.8205	45.1444
1500	230.387	212.297	32.4462	17.7462	207.7213	44.3234
1550	229.398	210.992	32.0356	17.3356	206.5757	43.4927
1600	228.427	209.709	31.6396	16.9396	205,4384	42.6519
1650	227.477	208.444	31.2567	16.5567	204.3196	41.7995
1700	226.545	207.308	30.9193	16.2193	203.2474	40.93
1750	225.633	206.068	30.5574	15.8574	202.1972	40.0527
1800	224.737	204.843	30.2069	15.5069	201.16	39.157
1850	223.858	203.634	29.8671	15.1671	200.1397	38.2473
1900	222.993	202.439	29.5373	14.8373	199.14	37.3232
1950	222.143	201.258	29.2175	14.5175	198.1405	36.6098
2000	221.308	200.097	28.9088	14.2088	197,1225	36.0083
2500	213.801	190.458	26.5621	11.8621	197,1225	30.2915
3000	207.362	181.754	24.7231	10.02306	181.1839	26.7457
3500	201.666	173.49	23 2008	8.50083	181.1839	23.6625
4000	196.528	165.723	21.9464	7.24638	169.9794	21.4053
4500	191.848	158.642	20.9355	6.23548	169.9794	19.6263
5000	187.559	152.523	20.1542	5.45418	161.8639	17.8988

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CCN CONVERSION: CCN NO. CCN --

Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

Sheet No. _ 143

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE
0	S. Oliver	12/30/93	J. Elliott	1/4/94		AND AND THE OWNER OF THE PARTY OF THE PARTY.		New York States and St	
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TIME (SECONDS)	SUMP TEMP (DEG-F)	VAPOR TEMP (DEG-F)	TOTAL PRESSURE (PSIA)	GAUGE PRESSURE PSIG (W/R 14.7 psia)	LEFT BOUNDARY TEMPERATURE HS#1 (DEG-F)	UCHIDA CONDENSING HTC (BTU/FT2-F-HR)
5500	183.616	147.184	19.5358	4.83585	161.8639	16.6032
6000	179.988	142.745	19.0641	4.3641	155.6648	15.7554
6500	176.648	139.006	18.6948	3.99481	155.6648	14.977
7000	173.571	135.898	18.3979	3.69794	150.6964	14.218
7500	170.733	132.916	18.1451	3.44506	150.6964	13.5119
8000	168.113	130.795	17.9567	3.25665	146.6402	12.8586
8500	165.691	129.033	17.7952	3.09517	146.6402	12.217
9000	163.452	127.492	17.6548	2.95485	143.3137	11.5736
9500	161.373	126.109	17.5286	2.82862	143.3137	10.9301
10000	159.437	124.908	17.4264	2.72641	140,5415	10.3544

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Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

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REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
0	S. Oliver	12/30/93	J. Elliott	1/4/94				THE RESIDENCE OF THE PARTY AND ADDRESS OF THE		E
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TIME (SECONDS)	STEAM+AIR ENERGY (6TU)	SUMP ENERGY (BTU)	TOTAL ENERGY (BTU)	AIR COOLER HT REMOVAL (BTU)	CONT. SPRAY HEAT TRANSFERRED TO SUMP (BTU)	HEAT SINKS (BTU)
0.05	24175100	0	24175100	0	0	15.6006
0.1	25014300	0	25014300	0	0	64.7074
0.2	26662100	0	26662100	0	0	294.816
0.3	28269200	0	28269200	0	0	693.704
0.4	29835500	73.6082	29835500	0	0	1405.75
0.5	31362100	213.542	31362300	0	0	2755.78
0.6	32852600	429.334	32853000	.0	0	4826.49
0.7	34308800	726.789	34309500	0	0	7648.92
0.8	35735600	1104.78	35736700	0	0	11183.1
0.9	37133100	1568.27	37134600	0	0	15423.2
1	38501100	2115.83	38503200	0	0	20353.7
1.1	39839700	2743.12	39842400	0	0	25912
1.2	41154300	3452.43	41157800	0	0	32083.5
1.3	42447300	4246.35	42451600	0	0	38866.8
1.4	43718700	5130.55	43723800	0	0	46272.8
1.5	44968300	6110.33	44974400	0	0	54359.2
1.6	46196200	7180.07	46203400	0	0	63078
1.7	47405800	8340.82	47414100	0	0	72412.1
1.8	48598500	9593.98	48608100	0	0	82355.4
1.9	49774400	10940.9	49785400	0	0	92902
2	50933500	12378.2	50945800	0	0	104033
2.1	52075700	13899.8	52089600	0	0	115699
2.2	53206800	15506.1	53222300	0	0	127884
2.3	54329100	17198.2	54346300	0	0	140585
2.4	55442500	18984.7	55461500	0	0	153836
2.5	56547100	20867	56568000	0	. 0	167665
2.6	57642900	22836.1	57665700	0	0	182025
2.7	58731600	24890.4	58756500	0	0	196885
2.8	59813900	27030.7	59841000	0	0	212243
2.9	60889900	29257.7	60919200	0	0	228093
3	61959500	31571.8	61991100	0	0	244432
3.1	63022800	33973.6	63056800	0	0	261255

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REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
0	S. Oliver	12/30/93	J. Elliott	1/4/94	The state of the s	PHASE TORS HAVE A COMMON TO COMMON A		THE RESERVE OF THE PROPERTY OF THE PROPERTY OF		EV
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TIME (SECONDS)	STEAM+AIR ENERGY (BTU)	SUMP ENERGY (BTU)	TOTAL ENERGY (BTU)	AIR COOLER HT REMOVAL (BTU)	CONT. SPRAY HEAT TRANSFERRED TO SUMP (BTU)	HEAT SINKS (BTU)
3.2	64079700	36463.5	64116100	0	0	278557
3.3	65130200	39053.3	65169200	0	0	296386
3.4	66174200	41747.5	66215900	0	0	314789
3.5	67211700	44546	67256300	0	0	333759
3.6	68242800	47446.5	68290300	0	0	353283
3.7	69268700	50438.2	69319100	0	0	373312
3.8	70290000	53520.3	70343500	0	0	393823
3.9	71306600	56693	71363300	0	0	414812
4	72318500	59956.8	72378500	0	0	436274
4.1	73325800	63311.5	73389100	0	0	458206
4.2	74328500	66757.5	74395200	0	0	480601
4.3	75326400	70294.9	75396700	0	0	503456
4.4	76319800	73923.9	76393800	0	0	526766
4.5	77308600	77644.5	77386200	0	0	550527
4.6	78292700	81457.1	78374200	0	0	574734
4.7	79272900	85360.5	79358300	0	0	599382
4.8	80249700	89347.1	80339000	0	0	624442
4.9	81222900	93433	81316300	0	0	649964
5	82192300	97634	82290000	0	0	676074
5.25	84600000	108629	84708600	0	0	743865
5.5	86984700	120319	87105000	0	0	815127
5.75	89347900	132701	89480600	0	0	889751
6	91693400	145746	91839200	0	0	967566
6.25	94021800	159403	94181200	0	0	1048290
6.5	96333100	173669	96506800	0	0	1131840
6.75	98622900	188539	98811500	0	0	1218140
7	100877000	204014	101081000	0	0	1307130
7.25	103094000	220186	103314000	0	0	1399240
7.5	105273000	237061	105510000	0	0	1494540
7.75	107411000	254593	107666000	0	0	1592800
8	109497000	272708	109770000	0	0	1693680
8.25	111530000	291387	111821000	0	0	1797050
8.5	113510000	310609	113821000	0	0	1902770
8.75	115441000	330358	115771000	0	0	2010730

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Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
0	S. Oliver	12/30/93	J. Elliott	1/4/94				The second secon		EV
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TIME (SECONDS)	STEAM+AIR ENERGY (BTU)	SUMP ENERGY (BTU)	TOTAL ENERGY (BTU)	AIR COOLER HT REMOVAL (BTU)	CONT. SPRAY HEAT TRANSFERRED TO SUMP (BTU)	HEAT SINKS (BTU)
9	117332000	350618	117683000	0	0	2120840
9.25	119185000	371376	119556000	0	0	2233000
9.5	120998000	392620	121391000	0	0	2347140
9.75	122775000	414338	123189000	0	0	2463160
10	124521000	436529	124957000	0	0	2581050
10.5	127918000	482700	128401000	0	0	2824230
11	131198000	531198	131729000	0	0	3077050
11.5	134376000	581768	134957000	0	0	3338350
.12	137453000	634151	138087000	0	0	3606980
12.5	140431000	688248	141119000	0	0	3882360
13	143316000	743961	144060000	0	0	4163930
13.5	146119000	801207	145920000	0	. 0	4451240
14	148840000	859908	149700000	0	0	4743850
14.5	151481000	919993	152401000	0	0	5041400
15	154047000	981554	155029000	815.367	0	5343480
15.5	156545000	1045880	157591000	9026.82	0	5649790
16	158983000	1111320	160094000	17335.5	0	5959740
16.5	161363000	1177750	162541000	25731.7	0	6272830
17	163690000	1245130	164935000	34213.6	0	6588840
17.5	165975000	1313420	167288000	42779.9	0	6907590
18	168215000	1382890	169598000	51428.8	0	7230250
18.5	170410000	1453690	171864000	60158.6	0	7557600
19	172564000	1525720	174090000	68967.9	0	7889250
19.5	174683000	1598940	176282000	77855.2	0	8224880
20	176766000	1673280	178440000	86819.3	0	8564220
21	180832000	1825250	182657000	104966	0	9253060
22	184780000	1980910	186760000	123394	0	9953310
23	188617000	2139630	190756000	142070	0	10662500
24	192345000	2301040	194646000	160983	0	11379000
25	195966000	2464970	198431000	180133	0	12102000
26	199483000	2631190	202115000	199513	0	12830400
27	202918000	2799460	205718000	219117	0	13563200
28	206276000	2969620	209246000	238940	0	14299600
29	209559000	3141290	212700000	258966	0	15038500

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Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

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REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
0	S. Oliver	12/30/93	J. Elliott	1/4/94		A PARTICULAR OF CHINAPPER COLOR OF A PARTICULAR OF THE PROPERTY OF THE PARTICULAR OF			****	EV
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TIME (SECONDS)	STEAM+AIR ENERGY (BTU)	SUMP ENERGY (BTU)	TOTAL ENERGY (BTU)	AIR COOLER HT REMOVAL (BTU)	CONT. SPRAY HEAT TRANSFERRED TO SUMP (B*U)	HEAT SINKS (BTU)
30	212767000	3314200	216082000	279178	0	15778700
31	215905000	3488210	219393000	299572	0	16519900
32	218986000	3663190	222650000	320144	0	17261500
33	222016000	3839070	225855000	340892	0	18003100
34	224994000	4015740	229009000	361812	0	18744400
35	227920000	4193140	232113000	382901	0	19485100
36	230795000	4371170	235166000	404156	0	20225000
37	233614000	4549590	238163000	425565	0	20963300
38	236375000	4728170	241103000	447113	0	21699300
39	239080000	4906840	243987000	468795	0	22432800
40	241728000	5085560	246814000	490611	0	23163600
41	244321000	5264260	249586000	512556	0	23891600
42	246863000	5442890	252306000	534629	0	24616500
43	249355000	5621400	254976000	556826	0	25338300
44	251797000	5799760	257597000	579145	0	26056900
45	254190000	5977910	260168000	601585	0	26772200
46	256534000	6155820	262690000	624141	0	27484000
47	258835000	6333460	265169000	646812	0	28192200
48	261094000	6511090	267605000	669597	0	28898000
49	263309000	6688890	269998000	692491	0	29602200
50	265481000	6866780	272348000	715494	0	30304500
51	267627000	7044660	274671000	738595	71196.4	31004300
52	269744000	7222390	276966000	761781	142029	31701100
53	271836000	7399950	279236000	785051	212468	32394800
54	273903000	7577290	281480000	808403	282518	33085100
55	275944000	7754370	283698000	831835	352181	33772000
56	277960000	7931160	285892000	855347	421463	34455400
57	279952000	8107620	288059000	878938	490367	35135200
58	281918000	8283710	290202000	902604	558897	35811400
59	283860000	8459420	292320000	926344	627057	36483800
60	285778000	8634640	294413000	950156	694849	37152300
61	287614000	8809240	296423000	974029	762278	37816400
62	288969000	8982850	297952000	997951	829326	38475100
63	289444000	9154820	298599000	1021900	895938	39126500

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REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
0	S. Oliver	12/30/93	J. Elliott	1/4/94						E
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TIME (SECONDS)	STEAM+AIR ENERGY (BTU)	SUMP ENERGY (BTU)	TOTAL ENERGY (BTU)	AIR COOLER HT REMOVAL (BTU)	CONT. SPRAY HEAT TRANSFERRED TO SUMP (BTU)	HEAT SINKS (BTU)
64	289259000	9324320	298583000	1045830	962035	39767800
65	288659000	9490970	298150000	1069720	1027580	40397900
66	287978000	9654610	297633000	1093570	1092550	41016500
67	287288000	9815320	297104000	1117370	1156950	41623700
68	286589000	9973060	296563000	1141110	1220780	42219500
69	285880000	10127500	296008000	1164790	1284030	42804400
70	285161000	10279200	295440000	1188420	1346710	43379000
71	284442000	10428200	294870000	1211990	1408790	43943500
72	283732000	10574700	294307000	1235490	1470300	44498300
73	283034000	10718600	293753000	1258940	1531220	45043500
74	282349000	10860200	293209000	1282340	1591580	45579500
75	281674000	10999400	292673000	1305670	1651360	46106500
76	281010000	11136400	292146000	1328950	1710580	46624600
77	280357000	11271100	291629000	1352180	1769230	47134200
78	279715000	11403600	291119000	1375350	1827310	47635400
79	279083000	11534100	290617000	1398460	1884830	48128400
80	278462000	11662400	290124000	1421530	1941790	48613400
81	277850000	11788800	289639000	1444540	1998180	49090700
82	277248000	11913200	289161000	1467490	2054020	49560400
83	276655000	12035700	288691000	1490400	2109310	50022600
84	276072000	12156300	288228000	1513260	2164040	50477700
85	275497000	12275100	287772000	1536060	2218210	50925600
86	274932000	12392100	287324000	1558810	2271840	51366600
87.00001	274375000	12507400	286882000	1581520	2324920	51800900
88	273826000	12621100	286447000	1604180	2377470	52228900
89	273285000	12733200	286018000	1626800	2429490	52650600
90	272751000	12843700	285595000	1649370	2480970	53066000
91	272225000	12952600	285178000	1671890	2531900	53475200
92.00001	271708000	13059900	284768000	1694360	2582300	53878400
93	271197000	13165700	284363000	1716790	2632150	54275700
94	270694000	13270100	283964000	1739170	2681470	54667100
95	270198000	13372900	283570000	1761510	2730240	55052800
96	269709000	13474400	283183000	1783790	2778480	55432900
97	269227000	13574400	282801000	1806040	2826180	55807600

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Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
0	S. Oliver	12/30/93	J. Elliott	1/4/94		SALE STATE OF THE SALE OF T		A STATE OF THE STA		E
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TIME (SECONDS)	STEAM+AIR ENERGY (BTU)	SUMP ENERGY (BTU)	TOTAL ENERGY (BTU)	AIR COOLER HT REMOVAL (BTU)	CONT. SPRAY HEAT TRANSFERRED TO SUMP (BTU)	HEAT SINKS (BTU)
98	268751000	13673100	282424000	1828230	2873360	56176900
99	268283000	13770500	282053000	1850390	2920000	56541100
100	267821000	13866500	281687000	1872490	2966110	56900100
105	265594000	14328300	279922000	1982510	3190500	58630900
110	263511000	14761200	278272000	2091460	3401930	60248100
115	261557000	15168300	276726000	2199390	3600570	61762200
120	259476000	15794300	275270000	2306400	3788520	63186400
125	257391000	16494200	273885000	2412810	3974100	64540900
130	255388000	17175100	272563000	2518710	4159070	65832400
135	253460000	17838800	271299000	2624110	4343450	67067300
140	251599000	18486900	270086000	2729030	4527240	68250500
145	249802000	19120400	268922000	2833500	4710430	69385900
150	248059000	19741100	267800000	2937520	4892980	70480000
155	246367000	20349800	266717000	3041110	5074910	71535400
160	244717000	20952200	265669000	3144320	5256300	72555300
165	243115000	21539400	264655000	3247230	5437220	73542800
170	241555000	22117500	263672000	3349740	5617570	74498200
175	240034000	22686300	262721000	3451870	5797350	75423600
180	238551000	23246100	261797000	3553630	5976570	76320600
185	237104000	23797400	260902000	3655010	6155260	77190600
190	235692000	24340600	260032000	3756040	6333410	78034600
195	234312000	24876000	259188000	3856720	6511050	78853900
200	232964000	25404000	258368000	3957060	6688170	79649500
210	230357000	26438700	256796000	4156740	7040680	81173500
220	227865000	27446000	255311000	4355040	7390920	82611500
230	225479000	28427900	253907000	.4551960	7738980	83969900
240	223191000	29386400	252578000	4747580	8084930	85255300
250	220993000	30323300	251317000	4941950	8428870	86473400
260	218878000	31240400	250119000	5135110	8770850	87629800
270	216840000	32138800	248979000	5327100	9110940	88729300
280	214862000	33026300	247888000	5518170	9449580	89780000
290	212952000	33893600	246846000	5708270	9786150	90783600
300	211106000	34745400	245851000	5897310	10120600	91740800
310	209318000	35582300	244901000	6085340	10453100	92655000

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REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
0	S. Oliver	12/30/93	J. Elliott	1/4/94						E
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TIME (SECONDS)	STEAM+AIR ENERGY (BTU)	SUMP ENERGY (BTU)	TOTAL ENERGY (BTU)	AIR JOLER HT REMJVAL (BTU)	CONT. SPRAY HEAT TRANSFERRED TO SUMP (BTU)	HEAT SINKS (BTU)
320	207585000	36405700	243991000	6272390	10783600	93529400
330	205902000	37216400	243119000	6458490	11112200	94366700
340	204267000	38015000	242282000	6643660	11439000	95169500
350	202676000	38802300	241479000	6827940	11764000	95940100
360	201128000	39578700	240707000	7011330	12087100	96679900
370	199622000	40344200	239967000	7193760	12408600	97389100
380	198157000	41099500	239256000	7375250	12728400	98069500
390	196729000	41845200	238574000	7555840	13046600	98723100
400	195336000	42581300	237917000	7735530	13362600	99351500
420	192640000	44028000	236668000	8092430	13988300	100547000
440	190047000	45444000	235491000	8446000	14605400	101673000
460	187548000	46831700	234380000	8796380	15214300	102737000
480	185122000	48199500	233322000	9144150	15815800	103750000
500	182778000	49539300	232518000	9489050	16409800	104712000
520	180511000	50855600	231366000	9831070	16996400	105624000
540	178313000	52149800	230463000	10170300	17575800	106491000
560	176182000	53423000	229605000	10506800	18148200	107316000
580	174104000	54678000	228782000	10840700	18713900	108108000
600	172074000	55915900	227990000	11172000	19273000	108872000
620	170096000	57136500	227232000	11500500	19825700	109604000
640	168167000	58340400	226507000	11826200	20372100	110306000
660	166284000	59528300	225812000	12149200	20912400	110981000
680	164446000	60700800	225147000	12469500	21446800	111629000
700	162648000	61858900	224507000	12787200	21975400	112254000
750.0001	158318000	64696700	223015000	13571000	23274400	113720000
800	154184000	67468100	221652000	14340700	24546500	115070000
850	150236000	70171900	220408000	15096400	25792600	116316000
900	146460000	72813900	219274000	15838300	27013400	117465000
950	142843000	75398100	218241000	16567400	28209800	118526000
1000	139392000	77925500	217317000	17282800	29383700	119492000
1050	136100000	80400000	216500000	17983800	30537200	120366000
1100	132950000	82825800	215775000	18671100	31671100	121160000
1150	129929000	85206300	215136000	19345300	32786100	121883000
1200	127047000	87524900	214572000	20007000	33882700	122543000

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REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
0	S. Oliver	12/30/93	J. Elliott	1/4/94		THE THE COMMISSION AND VALUE OF BUILDING TO BE		THE REAL PROPERTY OF THE PARTY		E
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TIME (SECONDS)	STEAM+AIR ENERGY (BTU)	SUMP ENERGY (BTU)	TOTAL ENERGY (BTU)	AIR COOLER HT REMOVAL (BTU)	CONT. SPRAY HEAT TRANSFERRED TO SUMP (BTU)	HEAT SINKS (BTU)
1250	124214000	89850400	214065000	20658300	34963300	123156000
1300	121511000	92115300	213626000	21298300	36026500	123712000
1350	118906000	94344000	213250000	21927500	37073200	124216000
1400	116394000	96538200	212932000	22546200	38103900	124673000
1450	113959000	98701100	212660000	23154900	39118800	125093000
1500	1599000	100834000	212433000	23753500	40118500	125480000
1550	109324000	102935000	212259000	24340800	41103100	125823000
1600	107129000	105006000	212135000	24917000	42073100	126128000
1650	105007000	107049000	212056000	25482800	43029000	126399000
1700	102947000	109067000	212015000	26038900	43971900	126641000
1750	100945000	111062000	212007000	26586000	44902300	126860000
1800	99005400	113031000	212036000	27123700	45819700	127050000
1850	97124600	114976000	212101000	27652400	46724500	127214000
1900	95299400	116899000	212198000	28172400	47616800	127354000
1950	93529500	118799000	212328000	28683600	48496900	127470000
2000	91819800	120676000	212495000	29185200	49365100	127559000
2500	78724400	138268000	216992000	33820400	57537900	126000000
3000	68454600	154504000	222959000	37801700	64851600	123626000
3500	59999000	169650000	229649000	41188700	71387400	121123000
4000	53155500	183835000	236991000	44069500	77214100	118474000
4500	47730200	197170000	244900000	46509200	82398700	115698000
5000	43498500	209771000	253270000	48574200	87016100	112837000
5500	40245000	221767000	262012000	50324300	91141800	109919000
6000	37736000	233257000	270993000	51831200	94856400	107005000
6500	35772200	244338000	280110000	53145700	98222100	104146000
7000	34200500	255095000	289295000	54299100	101299000	101381000
7500	32923400	265579000	298502000	55326000	104131000	98721500
8000	31880000	275829000	307709000	56240600	106755000	96173900
8500	30988400	285900000	316888000	57054300	109209000	93754000
9000	30189100	295827000	326016000	57787000	111526000	91467400
9500	29467900	305627000	335095000	58448400	113722000	89300700
10000	28881500	315308000	344189000	58988000	115810000	87240100

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REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE
0	S. Oliver	12/30/93	J. Elliott	1/4/94			-	SCHOOL SECTION	

11 MASS AND ENERGY BALANCES

To ensure the reasonableness of the results, mass and energy balances were performed. The following tables show a mass balance at 102% power with offsite power available and a energy balance at 102% power with offsite power available.

A review of these tables indicates that the COPATTA Code mass and energy inventories rarely differ by more than 0.01 percent. This fact verifies that the mass and energy input parameters have been properly conserved within the COPATTA Code logic.

The data in the energy balance table is part of the data that is presented in Table 6.2-15D of the UFSAR.

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CCN CONVERSION:

Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

Sheet No. 153

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
0	S. Oliver	12/30/93	J. Elliott	1/4/94		AND SAME OF THE PERSON OF THE		Water and State of St		E
										U

MASS BALANCE	I	ELAPSED TIME SIN	CE BREAK (seconds)
	50 ^(b)	62 ^(c)	71 ^(d)	10,000 ^(c)
PROGRAM INPUTS(4)				
Initial Water Vapor	6.809092	6.809092	6.809092	6.809092
Initial Air	163.1983	163.1983	163.1983	163.1983
Break Flow (CS 301)	233.393	261.815	263.899	263.899
Ctmt. Spray Flow (CS 801)	0.0	2.67334	4.67834	2216.64
Total Program Input	403.400	434.496	438.585	'2650.546
PROGRAM INVENTORY(a)				
Steam	209.460	232.036	230.336	11.9598
Air	163.198	163.198	163.198	163.198
Sump	30.7450	39.2655	45.0539	2475.39
Total Program Inventory	403.403	434.500	438.588	2650.548
Difference In Totals ^(a) with respect to Program Inputs	-0.003	-0.004	-0.003	-0.002
Percent Difference with respect to Program Inputs	-0.00074	-0.00092	-0.00068	-0.000075

Notes:

- (a) All mass inputs and inventories are presented in 1000 pound increments.
- (b) The time of 50 seconds corresponds to the establishment of a fully developed containment spray injection phase flowrate of 1612 gallons/minute.
- (c) The time of 62 seconds corresponds to the nearest output time step for the occurrence of the containment pressure peak of 58 psi at time 62.3 seconds. GB 410/94
- (d) The time of 71 seconds corresponds to the nearest output time step for the occurrence of the end of mass release at 71.08 sec.
- (e) The time of 10,000 seconds corresponds to the end of the code run.

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CCN CONVERSION: CCN NO. CCN --

Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
0	S. Oliver	12/30/93	J. Elliott	1/4/94				ALCOHOLOGICA CONTRACTOR ASSESSMENT OF THE STREET		E
										1

ENERGY BALANCE	A STATE OF THE PARTY OF THE PAR	LAPSED TIME SIN	CE BREAK (SECON		
	50 ^(b)	62 ^(c)	71 ^(d)	10,000(6)	
PROGRAM INPUTS(a)					
Initial Water Vapor/Air	23.3257	23.3257	23.3257	23.3257	
Break Flow (CS 301)	280.043	313.921	316.383	316.383	
Ctmt. Spray Flow (CS 801)	0	0.181768	0.318094	150.716	
Total Program Input	303.369	337.428	340.027	490.425	
PROGRAM INVENTORY(a)	- 13-4 F				
Steam	240.903	264.974	261.082	12.5760	
Air	24.5774	23.9952	23.3600	16.3054	
Ctmt Atmosphere (Steam + Air)	265.48	288.97	284.44	28.88	
Sump	6.86678	8.98285	10.4282	315.308	
Structural Heat Sinks	30.3045	38.4751	43.9435	87.2401	
Air Cooler	0.715494	0.997951	1.21199	58.9880	
Total Program Inventory	303.367	337.425	340.034	490.418	
Difference In Totals ^(a) with respect to Program Inputs	0.002	0.003	0.007	0.008	
Percent Difference with respect to Program Inputs	0.00050	0.00089	0.0021	0.0015	

- (a) All energy inputs and inventories are presented in one million BTU increments. Reference temperatures for energy inventories are 32 °F for water and steam, 0 °R for air, and 120 °F (initial containment temperature) for structural heat sinks.
- (b) The time of 50 seconds corresponds to the establishment of a fully developed containment spray injection phase flowrate of 1612 gallons/minute.
- (c) The time of 62 seconds corresponds to the nearest output time step for the occurrence of the containment pressure peak of 58.5 psis at time 62.3 seconds. 6131-10-94
- (d) The time of 71 seconds corresponds to the the nearest output time step for the end of mass release at 71.08
- (e) The time of 10,000 seconds corresponds to the end of the code run.

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Project or DCP/MMP SONGS Units 2 & 3 Calc. No. N-4080-027

CCN CONVERSION: CCN NO. CCN --

Subject CONTAINMENT P/T ANALYSIS FOR DESIGN BASIS MSLB

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REV	ORIGINATOR	DATE	IRE	DATE	REV	ORIGINATOR	DATE	IRE	DATE	R
0	S. Oliver	12/30/93	J. Elliott	1/4/94		Printer Section and Control of Co		AND AND THE OWNER OF THE OWNER,		E
NAMES OF TAXABLE PARTY.	Company of the Compan		THE COMMENT OF THE PARTY OF THE PARTY.			PARTIES THE PROPERTY OF THE PARTIES AND ADDRESS				1

APPENDIX A (COPATTA Code I/O File Information)

The COPATTA Code input file is presented in Section 9 (page 130) of this calculation.

The COPATTA Code output file is included on Microfiche. The output file name and date are as follows:

FILE TITLE:

MSLB CASE, 102% POWER, LOSS OF ONE COOLING TRAIN,

OFFSITE POWER AVAIL.

RUNDATE:

11-1-93

END OF RUN: 09:47:46

LAST SHEET: Page 414