

BACKGROUND INFORMATION FROM KIRKPATRICK'S FILES

- K-1 Notes from TMI Computer Surveillance Leak Rate Test Sheets.
- K-2 Notes of Water Additions from CRC Log.
- K-3 Change to Leak Rate Test Procedure dated 3/16/79.
- K-4 TMI 1 Leak Rate Test Procedure 1303-1.1 Rev. 7 dated 05/25/76.
- K-5 Calculator printer strip with program and data from leak rate calculations done in 1980.
- K-6 Copy of RCS Leak Rate Hand Calculation dated 08/19/77.
- K-7 Reactimiter data for Rx Trip of 03/28/79.
- K-8 History of Rx power August 30 to November 30, 1979.
- K-9 RLS Pressure from Narrow Range Strip Chart.
- K-10 Proposed IE Bulletin on Leak Rate Testing (Was not issued).
- K-11 NRC Program Used to Calculate 24 hour Leak Rates.
- K-12 Notes on Discussion with J. Floyd.
- K-13 Hand Calculations and Calculator Notes.
- K-14 Notes on Discussion with B. Smith.

8410180207 841001
PDR ADOCK 05000289
G PDR

K-1

K-1 Notes from ^{TIII} Computer surveillance
break into Test sheets

Date	Time	Indy mol	Open change DSH	Open change DSH	ID Leaky DS3	OTSG Tide Leak	TAVE Asfor Ages	PZR LV By Ages	MJT LV By Ages	ROOF LV By Ages	Seal Rate GPM	ZOI Rate GPM	VID Rate GPM	Type of test	Comments
1/2/74	17:28	0103	0	0	-12	0	581.409 325.009 328	87.728 174	76.101 359	1.0784	.5735	-1151	C	100 added 900-130-6 100	
1/11/74	23:28	1	0	0	0	0	581.200 262.752 555.266 688	62.153 76.464 65.982 76.205	.5630	.3510	.2121	C	0320 added 900 Denim To MU-T typically entire in bag at end of each period		
1/15/74	23:17	1	0	0	0	0	582.219 202.788 586.225 879	65.424 77.694 65.263 78.091	1.1907	.4040	.6507	C			
1/16/74	17:15	1	0	0	0	0	581.000 205.746 584.453 346	75.409 76.061 591 665	.1084	.6083	.5204	C	also got water at 70.28 and 79.19 AOK		
1/17/74	11:10	1	0	0	0	0	581.205 205.234 584.888 888	74.216 76.659 88.203 995	.2034	.4242	.2108	C			
1/16/74	21:33	1	0	0	0	0	581.205 205.234 584.888 888	74.216 76.659 88.203 995	.443	.3448	.6378	C			
1/16/74	18:44	1	0	0	0	0	581.205 205.234 584.888 888	74.216 76.659 88.203 995	1.9680	.5730	.8330	C			
1/11/74	21:28	1	0	200	.085	0	581.205 205.234 584.888 888	74.216 76.659 88.203 995	.587	.5205	.1688	C	20 gal Denim for MVT / 2.2.29 - 2.2.130 Completed by first 4000 y Done by Hartman		
1/15/74	24:30	1	0	0	0	0	581.205 205.234 584.888 888	74.216 76.659 88.203 995	.8417	.5778	.2639	C	100 added 900-130-6 100		
1/20/74	6:54	1	0	0	0	0	581.205 205.234 584.888 888	74.216 76.659 88.203 995	1.6889	.7121	.9867	C	no data 1/15 - 1/10 Shut down?		
1/20/74	6:54	1	0	0	0	0	581.205 205.234 584.888 888	74.216 76.659 88.203 995	1.5111	.8107	.1003	C			

Feb 49	FAVE	PRR	NOT	RCOT	PRR	Cementin
Date	By	LVL	LVL	LVL	By	Trans Lbr
Time	Apt	By	By	By	ID	and leather
	Apt	Apt	Apt	Apt	UID	addition of
		apt	apt	apt		and/or other
24:31:59	582.461	225.414	67.021	76.090	.1246	another topic
	.391	.477	66.816	.950	.0752	at 0155
3	582.016	224.395	74.157	88.525	.0752	another at
10:32:18	.388	5.826	73.373	81.579	1.0657	5:17 and 23:49
4	582.203	225.914	62.258	76.082	.9670	
4:45:2	.594	6.564	10.545	.903	1.0274	
5	581.945	225.725	68.100	79.256	.0604	also at 8:33
18:37:2	582.938	224.752	63.187	80.270	1.1607	and 3:12
6	581.813	226.385	74.440	78.087	1.8431	
0:25:40	582.156	229.674	70.933	79.101	1.1830	
7	581.805	218.949	77.420	78.247	.6601	
11:50:35	582.000	217.857	75.665	79.326	2.1020	also 15:52
8	581.711	218.600	74.287	97.102	1.2594	
1:0:44	.891	219.648	76.345	78.130	1.2746	also 20:49
10	571.556	225.881	71.857	76.888	.4235	
8:48:16	572.094	.842	70.211	78.010	2.1705	
11	581.781	225.961	69.382	76.109	1.4028	
2:41:5	.680	.586	66.661	.956	1.4028	also 18:05
12	580.773	224.654	65.570	75.802	1.0579	added 300 to
21:20:19	581.016	226.070	.058	.446	.7610	RCs w/o making
13	581.164	224.893	73.482	75.512	.4849	
18:42:28	.156	225.445	70.326	76.628	2.0404	also 12:36
14	581.055	226.863	75.462	77.131	1.3539	
6:30:46	.266	225.936	79.716	78.341	1.6864	also 20:45
15	581.117	226.025	73.486	78.345	1.2401	also 20:45
20:26	.266	.141	70.482	79.859	1.4842	REC 206
16	581.086	226.588	76.295	76.346	1.5340	
12:03	.516	227.650	79.565	77.727	2.4653	also 2:53
17	581.214	226.846	67.878	77.219	1.7745	open course, 25
4:11	.078	225.852	63.816	78.906	1.7263	change 20:12
19	581.031	226.486	72.636	78.727	1.0482	
21:25	.125	224.370	.665	80.489	2.8772	also 1:34
21	581.031	221.318	72.520	77.178	2.0745	and 0:1
8:36	.289	.287	70.095	78.861	2.3785	
23	581.508	224.479	70.041	75.473	2.0325	
11:7	.305	228.807	66.782	.498	0.3463	By Hartman

15+12=30

Date	Time	Tare	PZR NVL A	MUT NVL A	RCDT NVL A	Leakage Cross I.D. U.I.D.	Comment
2/25/89		581.367	226.104	79.445	75.435	2.9974	OCC 150
2002		21.1	287	78.207	77.863	2.4058	5921
✓ 26		581.164	227.953	72.915	77.064	3.2577	OCC 154
78.39		328	227.945	095	79.143	2.4163	also 0.38
✓ 27		581.344	227.104	73.907	76.327	3.3372	OCC 162
21.50		469	135	428	78.253	2.3864	9507
✓ 28		581.117	227.117	74.628	76.846	3.2534	100 to MUT
79.9		367	228.020	77.853	78.983	2.5899	20.03-26.65
✓ 3/6		581.516	227.577	68.249	77.042	2.9831	(deleted H2)
0:41		492	228.790	69.404	79.184	2.5787	
✓ 5/2		581.016	226.727	66.641	76.457	3.2006	also 1.46
14:35		523	228.756	62.853	76.627	2.6611	
✓ 3		581.750	227.029	79.495	76.257	3.27738	OCC 152 DS4
21:38			226.301	79.503	78.238	2.4577	
✓ 4		582.000	224.564	84.433	76.805	2.8368	OCC 238 DS4
7:42		581.492	.162	449	79.177	2.8676	
✓ 5		581.633	226.025	68.187	76.271	3.6384	OCC 128 DS4
3:20		489	224.790	67.246	78.521	2.7684	
✓ 6		582.195	223.740	79.229	76.235	3.4874	OCC 180 DS4
3:21		581.852	224.227	77.807	78.435	2.7130	
✓ 8		582.063	227.242	73.466	76.250	3.5766	228 to MUT DS4
3:6		582.031	227.814	73.508	78.789	3.1087	also -0.05
✓ 9		582.203	228.734	67.783	75.849	4.3402	OCC 151 DS4
3:23		.156	260	66.153	78.692	3.4851	
✓ 10		582.039	226.498	81.366	76.563	4.0724	BY Hartman
3:51		.352	228.070	74.915	79.261	3.2674	
✓ 11		581.070	222.439	77.304	75.933	0.9817	OCC 200 DS4
21:53		844	227.756	81.745	76.410	0.7505	-1.585
✓ 12		581.773	228.141	71.812	76.147	3.9284	
11:32		430	227.215	65.520	79.166	3.6763	
✓ 13		582.078	228.023	64.982	76.608	3.6252	BY Hartman
2:00		.242	227.441	60.174	79.629	3.4407	
✓ 13B		582.383	228.885	71.736	76.769	4.3155	305 to hat
11:05		281	229.826	72.361	79.937	3.7894	11:55-1200
✓ 14		581.813	227.461	72.741	76.738	-0.7468	500 to RCDT
12:05		445	228.902	79.833	78.222	-6.4472	DS4

R+ cutback at 2029 on 0/17 - K-2

Water Additions from CRO LCA

Date	Time	Amount	Totals	Power Comments	Comments
9/18/78	0205	351 (BA)			What is
1	0325	250			BA
	0410	500		commenced Power increase	"De Greeting"
	0445	300			
	1005	450			
	1745				opened CA-V-4A/4B
	1835				shut CA-V-4A/4B
9/19/78	2400			15%	opened CA-V-4A/4B
2	0050				shut CAV 4A/4B
	0215	200			
	0255	300			
	0400	200			
	1630				opened CA-V-4A/4B
	1650	800			
	1707				shut CA-V-4A/4B
	1740	815			
	2212	Commenced	SD from cutback & Rm.		
9/20/78	2217			Rx Trip	
3	0305			Rx Cutback	BA
	0614			Rx 14%	
	0800				opened CA-V 4A/4B
	0900				shut CA-V 4A/4B
	1606			Rx Trip	opened CA-V-4A/4B
	1915				shut CA-V-4A/4B
	2015				
	2115			Rx Cutback	

WATER ADDITIONS FROM CRO LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
9/21/78	0215			10%	opened CA-V-4A & B
4	0243			Rx 70p	shut CA-V-4A & B
	0530			Commenced Rx 50	
	1900	1000			
	2145	300			
9/22/78	0000			50%	"BFwd water valve seems to be the cause of the oscillations"
5	0245	600			
	0550	600			
	0645	700			
	0328			Rwd load 22%	
	0700			30%	
	0815				opened CA-V-4A & B
	0855				closed CA-V-4A & B
	0925			15%	
	1120			Rx at 10 ⁻⁸ A	
	1145	100			
9/23	0000			10 ⁻⁸ A	
6	0250	266 (BA)			From RCRT From 3A 4T
	0530				RCS Press 150
	0900	4000			from "C" RCRT
	1045	400			from C RCRT
9/24	0000			CSD	
9/24	2300				2000 psi, at 485 °F
7	2330				Commenced elaboration. Running 1/4 V 5 clean water

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
9/25/80	0000			SID	deporting
8	0645			R/Critical	
	0915			Comence raising WA	Commenced raising power to 5% causing power
	1510			18%	
	2056			R Trip	
	2330	450			
	2350	1050			
9/26	0040			Cut at 10-8%	
4	0050	850			
	0245				opened CA -V 4A & 4B
	0315				shut CA -V 4A & 4B
	0700			20%	Completed 2301-301 ID, 2300
	1841				UID .7287
	1930	1000			
	2300			150 MWE	
9/27	1640	1000			
10	2300			26%	(1st stable day) 231 MWE
9/28	0915	150			
11	0936			↑ 30%	
	1230			↑ 50%	
	1820	160			
	2010	200			
	2115				Completed SP 2301-301 .0914 GPM
	2124	205			UID
	2300			40%	

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WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
9/29/78	1602	200		40%	
12	1955				Completed 2301-301 .6704
	2300			40%	
9/30/78	0023	211			
13	0232				Comp 2301-301, 3393 GPH U/D
	1511	200			
	"	-200*			*Bleed 200 gpm from RCS to B' bleed Tr
	1700	350 BA			
		200			
	1830				Comp 230-301, Leak Rate Sat
	1845	200 ^{from} _{C' bleed}			
	2300			40%	
10/1	0030				Comp 2301-301. Sat.
14	0440	200			
	1430				Add H ₂ to MVTR
	1540				Stopped adding H ₂ to MV-T-1
	2035				Comp 2301-301 .1775 gpm U/D
	2300			40%	
10/2	0030	312			
15	1640	457			From "C" RCBT
	"	143			
	1914	100			
	2300			40%	
	2310				Completed 2301-301 sat.

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
10/3/78	0830	600			
16	1740	200			From RCBT "C"
	1822	200			From RCBT "C"
	2235				Commenced feeding H ₂ to makeup tank
	2300			40%	
10/4/78	1555	285			From RCBT "C"
17	"	85			
	2255			40%	
10/5	1445	145			Leak Rate .96 gpm VED
18	0150	250			
	0800				Opened CA-V-4A 2B
	0900				Shut CA-V-4A 13
	1301	???			Raised MUTX Lvl to 85" from "B" ^{RCBT}
	1430			Rx Trip	Manual
	1903	???			Completed adding Required BA to ACS
	2300			on cooldown	
10/6				SD	
10/7				SD	
10/8				SD	
10/9				SD	
10/10				SD	
10/11				SD	
10/12	0000			SD	
	2300			10%	
	2355				opened CA-V 4A/13

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
10/13	0035	200		10%	CA-V-4A/B is still open
19	0152	200			close CA-V-4A/B
	0315	200			
	0340	400			
	0435	450			
	0500	600			From "B" RCIBT
	0517	230			" " "
	0625	500			
	1333			↓ 10%	
	1530			↑	Began raising power
	2300			20%	
10/14	0215	682			
20	0422	400			
	0702	500			
	0720			Rx Trip	
	1025				Opened CA-V-48 & 413
	1100				"Pumped Down RC Drain Tank 47-75" Thred time since Trip
	1123				Closed CA-V-4A & B
	1536			Rx Trip	Critical at 1555
	1615				Opened CA-V-4A & B
	1940			Rx 20%	
	2300			Rx 35%	

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
10/15/78	0035			40%	
21	2300			40%	
	2350				Shut CA-V-4A, AB
10/16/78	0038	283*			from RCBT "B"
22	"	197*			
	0150	200*			
	0555	250*			
	0830	800*			From RCBT A and DI water
	1115				opened CA-V-4A/B
	1215				closed CA-V-4A/B
	1302	240*			
	1528	600*			
	1930	745*			from RCBT B
	2300			40%	
10/17/78	0155	650*			From RCBT "B"
23	0521				stopped adding ^{to effect on strip chart} 1/2 hr 40% From RCBT "B"
	0531	630*			
	0800			↓ 27%	at 5%/min.
	0828	400*		↑	
	0830			↑ 30%	
	0955	400*			manually tripped steels
	1025				
	1125	400*			
	1155			↑ 20%	

* correlated to strip chart.

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
10/17/18	1228			35%	
23	1310			↑ 40%	
23	1322			40%	
	2300			at 45%	
10/18	1325				Completed 2301-301 - 2839M
24	1822	450 *			Called this "Identified" rate
	2245				Added H ₂ to MVT brought it
	2300			50%	to ≈ 22#
	2300			50%	
10/19	0506			↑ 50 MW	
25	0720	100 *			
	0852				Completed 2301-301 UIDGO
	0920			57%	
	0927	500 *			From RCBT "B"
	"	122 *			
	1215	200 *			
	1310	200 *			
	1530	250		60	
	1700			↑ 60	
	1755	350 *			
	1935			↑ 63	
	2210				MUV-17 Picking, blowing out
	2221	350 *			from RCBT "A" (8) and Dwin (2)

2300

63%

correlates to trip chart

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
10/20	0214	.			Vented of MU-T-1
26	0230				Added More H ₂ to MUT-1
	0407	(± 463)			*Feed and bleed.
	0455			168%	
	0624	(± 440)			*Feed and bleed
	1821				main machine stopped?
	1927				Open CA-V-4A/B
	2015				Shut CA-V-4A/B
	2300			17%	
10/21	0148	426			From "A" bleed tank
27	0150				Ramped down RC down to 75"
	0325	325			From "B" bleed tank
	0420				Feed and bleed 700 gal
	510	200 BA			From B A MT
	0700	50 BA			" "
	0730	50 BA			" "
	0830	50 BA			" "
	0900				Added H ₂ to MU-T-1
	0930	200			"B" RC BT
	1125	50 BA			From B A MT
	1209	100 BA			" "
	1345				Completed 2301-301 06P17
	1501			17%	Started raising power to 75% from 55%
	1909				Turbine Trip Rx power back to 15%

*Correlated to ^{MUT} strip chart

over

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
10/21 ^{Control}	2115	3000			To maintain Pad/Hite Feed Albed?
	2155			20%	Raised Power to 20%
	2230	AD		↑ 28%	R
	2255				Rt Power to 40%
	2300			40%	#
10/22 ✓	0039	90 BA			
28	0230				Began inc power to 70%
	504			↑ 70%	
	0910				Leak Rate 2301-301 CGP4
	1105			↑ 115%	
	1355	200			strip chart
	1430	✓ 200			all over
	1535	✓ 400			
	1700	✓ 200			
	1840	✓ 200			
	1945	✓ 200			
	2057	✓ 200			
	2221	✓ 200			
	2236	✓ 200			
	2300			72%	
10/23	0525	✓ 100 *			
29	0600	✓ 400 *			241 gal from B RCBT & 109 from
	0710	✓ 100 *			

overlaid a strip chart

10/23 Control.

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
10/23/18	0800				Increased (H_2) over pressure
29	0845	100*			
	945	100*			
	1200	50			
	1305	100*			
	2300			73%	
10/24/18	0145	500*			1088 PPM (Prob ^a bleed tank)
30	1000				Added (H_2)
	2001	300*			
	2300			75%	
10/25/18	0448	450*			
31	1011	409*			"A" RCBT
	"	91			
	1717				Added (H_2) to MUT 2# increase
	1828	458*			RBT "A"
	"	102*			
	2300			75%	
10/26/18	0740	470*			Added (H_2) to MUT 25#
32	1235	200			Wild strip chart
	1536	100			
	1545	200			
	1548	200			
	1605	200			

Correlated w strip chart

10/26 cont'd.

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
10/26/78	1800	25 BA			Wild stuff chow
32	1830	25 BA			
	1850	200			
	1945	500			
	2116	25 BA			
	2200	600 *			"B" RCBT
	2300			75%	45%
10/27/78	0817	470 *			RCBT B
33	"	130 *			
	1803				Completed 2301-3D1 .176/gm
	2300			82.5%	
10/28	0125	300			
34	0145	300			
	0158			90%	started reducing power
	0640	400			
	0655	400			} reducing power liberating?
	0700	400			
	0710	600			
	0745	600			
	0858	600			
	0920	500			
	0930	300		8.5%	
	1229	200			

10/28 cont'd

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
10/25/78	1318	300			
34	1730	100			BAIT
	1937	25			BAIT
	2008	25			BAIT
	2035	25			BAIT
	2105	25			BAIT
	2150	35			BAIT
	2220	35			BAIT
	2255	35			BAIT
	2300			89%	
10/29/78	0211	330			BAIT to more rods out to 65% ^{0/1}
35	0345				Added H ₂ to MU-T-1
	0750	50			because of low H ₂ in RCS BAIT
	0850	100			BAIT
	1014	88			BAIT
	1140	88			BAIT
	1715			10 ⁻⁸ _h	
	1730	2000			RGBT "B"
	"	200			
	2300			Rx SD	
10/30/78	0613	480 ²			RGBT "B"
36	1235				2301-301, 8874 UID
	1310	600 ²			B bleed tank.

10/30 cont'd

WATER ADDITIONS FROM CRO LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
10/30/78	2150	350			BAIT
36	2300			SD	
10/31/78	0155	350			BAIT
37	1900	1000			'13" RC BT
	2300			SD	
	0124			Rx Ambient	15% at 0330
11/1/78	1020	420			
38	1420	440			
	1540	250			
	1615	210			
	1810	310			
	1838	600			
	2125	1200			
	2250	600			
	2300			54%	
	2345	500			
11/2/78	0130	500			
39	0431				Leak rate .8978 GPM
	"	1000			
	0559	500			
	0620	300			
	0637	500			
	0640			80%	
	650	500			

11/2/78 contd.

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
11/2/78	1130			90%	
39	1250			↓ 50%	Run back on loss of FNI?
	1414	✓ 900		40%	
	1515	✓ 600			
	1942	✓ 600			
	2010	✓ 1000		40%	
	2045			90%	
	2120	✓ 400			
	2145	✓ 300			
	2220	✓ 20			BAMT
	2240	✓ 20			BAMT
	2300			90%	
	2305	✓ 500			
11/3/78	0025	✓ 200			
45	0200	✓ 200			
	0220	✓ 200			
	0355	300			
	0610	300			
	0805	- 500			Balanced 500 gal to "O" ROBT
	0815	+ 500			
	1002	500			
	1325	200			
	1410	400			

11/3/78 contd.

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
11/3/78	1809	50			
40	1845	50			
	1915	50			
	2300			89%	Turb Trip R Trip, MFP's Trip Do
	2312	110			To all Condensate pipelines isolation
11/4/78	0448	3333		TRIP	Isolated 3333 gal to RCS
41	1435	1120 *			From RC BHT-113
	1645	450 *			From "B" RC B T
	1922	652 *			Boric Acid. from B A M T
	2220			Ry Cut	
	2235	100			
	2300			10%	
	2305	1400			
11/5/78	0115	25 BA			BA
42	0146	25			BA
	0340	75 BA			BA
	0445	50			BA M T
	0835	65			
	1225	275			
	1348	300			rechecked 00% at 1300 "Feed & Bleed"
	1520	300			
	1550	200			
	1618	200			

11/5 contd.

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
11/5/78	1702	300			
42	1730	1300			
	2015	800			
	2210	500			
	2230				added H_2 to MU-T-1
	2300			90%	
11/6/78	0152	1000			Completed 2301-310 / UID: 2774
43	0325	400			
	0445	400			
	0631	200			
	0930	600			"For Xe Control.
	1205	200			
	1615				MU Tank Level Transmitters LT-1
	17				and LT-2 are both recalibrated and
	1910	250			back in service
	"	200			"B" RCBT
	2040				Completed 2301-310 / UID: 2775
	2100	360			
	2140	200			
	2205	100			
	2240	50			
	2250			90%	
	2322	100		90%	
	2345	100			

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
^{C524} 11/14/78	0544			Rx Trip	K-T Trip
44	1016	2 RDS			St adding BA from BA4T
	1045	?			Secured adding BA
	1500				RCB Brown went from 1076 to 1202
	1750				Completed adding 8704 BA from BA4T
	2300			SD	
11/8	2045	800			.13345 PM Habsup
45	2300			SD	
11/9	0055				Commenced adding BA from BA4T
46	0400	763			BA (Secured adding BA)
	0415				Added (H2) to MUT
	1845	6			BA4T
	"	179			"B" RCBT
	2125	18			BA4T
		881			"B" RCBT
	2300			SD	
11/10	1516				Mode 5
11/11	2300				RC Press 290# Mode 5
11/11	2300				RC P 240# Mode 5
11/12	2300				Mode 5
11/13	2300				Mode 5
11/14	2300				Mode 5
11/15	2300				Mode 5

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
11/16	2300				Mode 5
11/17	2300				Mode 5
11/18	2300				Mode 5
11/19	2300				Mode 5
11/20	2300				Mode 3 at 350°F
11/21	2300				Mode 3 at 532°F
11/22	2300				Mode 3 at 350°F
11/23	2300				Mode 5
11/24	2300				Mode 5
11/25	2300				Mode 5
11/26	2300				Mode 5
11/27	2300				Mode 5
11/28	2300				Mode 5
11/29	2300				Mode 5
11/30	2300				Mode 5
12/1	2000				Commenced Rx 50
12/1	2300			13%	
12/2	1330			Rx Trip	On low pressure
12/2	2300			Mode 3	
12/3	1525			RxCrit	at 10 ⁻⁸ A
12/3	2300			47%	
12/4	0145	350			

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
12/4/78	0145	350			
47	0735			70%	2301-3101 complete "sat"
	1013	±100			Bleed & Feed.
	1040	±200			Bleed & Feed
	1050	±200			" "
	1110	±500			" "
	1120	±200			" "
	1225	±140			" "
	1300	±100			" "
	1344	±150			" "
	1410	±150			" "
	1435	±275			" "
	1715	4500			
	1758	4000			
	1830	1000			
	2230	250			
	2300			87%	
12/5	0615				RCS Leak Rate .8993
48	0905	200			
	0928	200			
	1100	200			
	1215	200			
	1410	100			

12/5 cont'd.

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
12/5/78	1700	200			(MUT stud.)
	2300			91%	Chart
12/6/78	0045	300			Wile
49	0325	200			"A" RCBT (since stop)
	0416	200			"A" RCBT
	0545	450			"A" RCBT
	0900	250			
	0925	100			
	1515	800*			
	1525	100*			
	2015				Head Rate Set (0.7713 gpm)
	2300			40	
12/7	0531	300*			
50	0810	20			BA
	0825	24			BA
	2005	50			
	2028	100			
	2115	100			
	2136	100			
	2210				Added 1/2 to MUT
	2300	4		90%	
12/8					

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
12/8/18	0135				LEAK Rate UID .6998 ID .424
51	1510	200			
	1730				Completed 2301-301 Leak Rate
	1815	400*			"B" RCBT
	"	100*			
	1945	(-200)			Feed and Bleed
	2000	(-200)			" "
	2057	(-200)			from "B" RCBT
	2300			90%	
12/9	0034				Completed 2301-3101 UID .4127
52	1148				UID .1872 Completed 2301-3101 "Sat"
	1655				Completed 2301-3101 .2607
	1710	400 gal			"B" RCAT
	2250			90%	
12/10	0000				Leak rate "Sat" .0879 UID
53	1103	(+700)			Feed & Bleed
	1208	(-374)			" "
	1230	(-500)			" "
	1315	(-500)			" "
	1340	(-300)			" "
	1520				Added (H ₂) to MU-T-1
	1605	100			
	1632	100			

Shut plant
 12/9/18

12/10 center

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
12/10/48	1815	100			
53	1930				2301-301 hot
	2300			90%	
12/11/48	0129				Completed 2301-301 G _{max} = .843
54					ID .1556 UID .6875
	0401	300 *			
	1825				Completed 2301-301 "hot"
	2000	100			
	2255			90%	
12/12	0400	500			
55	0430	500			
	0515	50 BA			BAAT
	0725	1300			"B" bleed tank
	0930	300			"B" bleed tank
	1135				Commenced reducing PWR to 55%
	1603	100			
	1640	(-200)			Feed and bleed 200
	1812	100			"B" PCBT
	1850	200			" "
	1930	300			" "
	2000	35			BAAT
	2200	30			BAAT
	2215	40			BAAT
	2235	25			BAAT
	2300			55%	

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
12/15/48	0708				Completed 2301-3121 SAT
58	0725	✓100*			
	1145	✓300*			"A" RCIBT + DEMIN
	1550	✓300*			A bleed TK and Demin water
	2215	✓600*			A " " " "
	2300			55	
12/16	0000			Commenced SD	
59	0225			R+at 10*	
	2300			Mode 3	Tang 533
12/17	0145	✓500			Completed SP 2301-3101 sat, 48320A
	0225	✓80			
60	1200	✓650			
	2020	✓100			BAMT
	2300	✓811		Mode 3	Tang 382
12/18	0915				Commenced adding BA 681 gal
61	1025				to 4VF-1 Completed addition
	1035				
	2300			Mode 3	Completed 230 Mode 3 at at 320F
12/19	0145	800			"A" RCIBT
62	2300	800		Mode 3	at 470°F
12/20	2300			Mode 3	Mode 3 at 533°F
12/20	1110	450			"A" RCIBT
63	2300			Mode 3	533°F
12/21	0425	750/301			Peak Rate sat 2301-30
64	0955				Commenced Debating
	1025				see Debating.

12/21 contd.

84
112

Date	Time	Water Additions (gallons)	Records of Power.
12/24/78	0135	300	57 0000
65	0220	300	930-945
	0245	300	97
	0540	300	2.523
	0840	280	
	1210	200	
	1225	125	
	1437	200	
	1450	200	
1730	1830	200	
	1900	200	946 97
12/25/78	0240	200	
25	1300	800	1.356
66	"	200	
	1600	200	
12/26/78	0500	100	1.960
67	644	130	96
	0855	50	
	1040	125	
	1925	134	
	1930	350	
	1950	200	
	2100	35	98
12/27/78	0300	300	1.4497
68	1135	400	
	"	100	
	1630	300	96
	1708	100	
	1905	100	
	1935	100	
	2000	100	
	2230	100	1.54400 (4448)
Start 12/28/78	0322	463	1.847 for
to 12/30/78	1250	400	Period
			96
			1500-96

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
12/3/18	120	300		80%	
69	309	600			
	0440	600			
	1145	200			
	0815	200			
	0845	200			
	1045	200			
	1130	350			
	1330	320*			
	1430	225*			(F & B per SC)
	1800	200*			
	1850	200*			
	2300			82%	
1/1/19	0030	300*			
70	0100	200*			
	0800	300*			
	1200	✓200			Noisy SC
	1510	✓200			Noisy SC
	1541	✓150			
	1825	RR			added H ₂ to AVT
	2105	400			
		400			
	2105	500*			

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
1/2	0040	350*		83%	
71	0745	200			F&B re SC
	1000	300			Large pumps
	1010	300			" "
	1025	400			" "
	2300		2200	52%	
1/3	0320	286			BANT
72	0815	600*			RCBT
	150	150			Remin
	1250	300			
	1325	(250)			F&B
	1420	200			
	2035	400			
	2300		2200	40%	
1/4	0225	300			
73	0300	400*			F&B re SC
	0715	500*			
	1030	50			
	1120	150			Large pumps
	1157	150			" "
	1920	500*			" "
	2200	200*			" "

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
1/5	0746	200		90%	
74	1020	200			
	1100	200			
	1115	300			
	1145	200			
	1200	(200)			F&B
	1445	20			
	1520	25			
	1600	25			
	2300			95%	
1/6	1135	100			
75	1157	(100)			F&B
	1215	(100)			F&B
	1919				2301-301 Sat.
	2300			92%	
	2330	100*			
1/7	0125	600*			
76	0312	100*			
	0740	100*			
	0955	467*			
	"	133*			
	1834	436*			
	"	130			
	2010	200			

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
1/7	2320	.		90%	
1/8	0255	600*			
1/7	0510	200*			
	0914	100*			
	"	50			
	1050	50			
	1115	50			
	1150	50			
	1715	500* 1			
	2245	500*			
1/9	2300			90%	
28	1251	600*			
	1710	450*			
	2140	200*			
	2210	200*			
	2242	200*			
1/10	0350	200*		60%	
29	1445	57			BA
	1800	200			
	2033	500*			
	2300			60	
1/11	0146				Added 1/2 2 1/2 bottles 154
	0240	400			
	0405	400			
	0945	1020			
	1040	1000			
	1115	410			

WATER ADDITIONS FROM CRC LOG

DATE	TIME	AMOUNT	TOTALS	POWER	COMMENTS
2/21/16	1430			4%	
	1200			4%	
1/11	0145			60%	Added H ₂ O to battery 15#
80	0240	400*			
	0455	400*			
	0945	102*			} Feed and bleed
	1040	1000*			
	1115	410*			
	1500	25			
	1145	400*			
	"	200*			
	1825	(200)			F&B
	2005	485*			
	2300			90%	2301 - 3D1 Lat 1.1688gph

Date	Time	Water in	Sampling	Power
12/28	1345 1345	700 300		
	1500		at 1522	
			Power evolution FW Pump Trip	
1/1/99	0700			
				TRIP To 83% only 1/2 - 6 To 90% 1/4 29 to 100% 1/19
1/10/19	0000		START	
	0300	200		
	1445	57		
	1800	200	1.024	60%
	2033	300		
1/17/19	0700	100	END	
12/1/19	0740	400		
	0445	400		Varies
	0945	1020		?
	1050	1000		
4/11 only	1115	410		
	1500	25		
12/23, 24, 25				
1/12, 13, 14				
1/31	2/1, 2			
2/10, 11, 12				
2/22, 23, 24				
3/18, 19, 20				

Date	Time	Water in	cf/s/Day cf/s	1/11 - 1/14
1/12/79 81	0300	388*	90%	3.0985
	"	211*		
	5.45	290*		
	6.15	200*		
	09.05	200*		
	09.15	200*		
	09.25	200*		
	09.55	200		
	10.50	200*		
	13.24	400*		
	18.05	450*		
	"	150*		
	20.35	100*		
	"	100*		
1/13/79	0130	600*		3.0194
	0610	600*		
	1000	117*		
	1200	900*		
	2145	900* / END		
1/14/79	0430	600		3859 for Period

raining

211 111

Date	Time	Water add Gal	alc Power	
2/3/79 82	0000	ST	92	5.58
	0215	300		145
	0245	300		Feed & Bheel
	1705	600*		
	2112	300*		
2/4/79 83	0135	450*		
	0432	300*		
	1116	656*		
	1915	600*		
	2050	200*		
2/5 84	0210	200*		
	0515	200*		
	0600	150*		
	1007	350*		
	1353	300*		
	1718	300*		
	2030	100		} noisy
	2115	100		
	2130	100		
	2320	150	END	
2/6 2/7	0000	END		
2/8 85	0000	9T	89	lots of F&B
	0025	200*		1695
	0205	150*		noisy
	1250	200*		noisy
	1750	200*		
	1800	200*		
	1825	200*		
	1845	200*		
	1900	200*		
	2330	200*		
2/9	0000	End		

Date	Time	Water	alc sewer	
2/12/79	0000	start	90%±2%	2.156
86	0755	200 *		
	0810	(200) *	} Feed E Bleed	
	0825	(200) *		
	1058	200 *		
	1428	300 *		
	1435	200 *		
	1750	626 *		
2/15/79	2345	300 *		
2/13/79	0130	300 *		1.655
87	0955	200 *		
	1210	150 *		
	1435	200 *		
	1700	469 *		
	1700	190 *		
	2225	200 *		
2/14/79	0720	70 *		1.293
88	0755	160 *		Forward during noon
	0942	55 *		0125-500 *
	1210	400 *		0100-200 *
	1635	100 *		0545-200 *
	1645	50 *		
	1705	50 *		
	1740	50 *		
	1825	400 *		
2/15/79	0125	500 *		2.945
89	0200	200 *		
	0545	200 *		
	0915	600 *		
	1345	600 *		
	1845	400 *		
	2315	300 *		
	2345	240 *		
2/16/79	0405	300 *		1.889
90	0415	250 *		
	0745	200 *		
	0825	200 *		

Date	Time	Water	of Pounds	
2/16/79 90	1033	100 *	90% ± 2%	
	1050	100 *		
	1110	100 *		
	3 hrs missing 1201-1500			Found on return 1250-204 *
	1505	200 *	1400-200 *	
	1850	200 *		
	2050	300 *		
2/17/79 91	0000	350 *	2.373	
	0920	400 *	Om Re Ex 0740-150 *	
	1122	200 *		
	0150	250 *		
	1520	250 *		
	1845	500 *		
	2230	500 *		
2/18/79 92	0245	541 *	2.349	
	"	234 *		
	0415	200 *		
	0635	200 *		
	0807	150 *		
	0854	150 *		
	1025	100 *		
	1320	150 *		
	1455	100 *		
	1550	200 *		
	2005	200 *		
	2225	200 *		
2/19/79 93	0305	500 *	2.479	
	0750	300 *		
	1000	306 *		
	1025	201 *		
	1137	152 *		
	1545	500 *		
	2000	100 *		
	2115	500 *		
2/20/79 94	0030	236 *	3.894	
	"	540 *		
	0355 com	200 *		

Date	Time	Water	ala Paculy
2/20/79 cont.	0435	150 *	90% ± 2%
	0455	200 *	
	0530	200 *	
	0555	200 *	
	0608	200 *	
	0625	200 *	
	0700	200 *	
	1430	594 *	
	1610	400 *	
	1820	200 *	
	2203	350 *	
	"	150 *	
2/21/79 95	0210	550 *	3.196
	0415	450 *	
	0630	500 *	
	1154	555 *	
	"	245 *	
	1815	200 *	
	1850	500 *	
	2130	100 *	
	2340	200 *	
2/22/79 96	0000	300 *	3.698
	0026	300 *	
	0100	300 *	
	0240	200 *	
	0640	117 *	
	"	271 *	
	0920	300 *	
	1115	400 *	
	1217	200 *	
	1440	300 *	
	1740	420 *	
	"	180 *	
	2015	180 *	
2123	200 *		
	2245	150 *	
2/23/79 97	0012	300 *	3.390
	0300	350 *	
		cont.	

Date	Time	Water	alc Power
2/23/79 cont.	0550	500 *	90% ± 2%
	0720	250 *	
	1135	150 *	
	1445	150 *	
	1550	450 *	
	1800	100 *	
	1836	100 *	
	1955	150 *	
	2110	200 *	
	2244	418 *	
	"	182 *	
	2335	200 * ✓	
2/24/79 98	0623	200 *	3.353
	0722	800 *	
	0852	205 *	
	0943	417 *	
	1305	400 *	
	1525	150 *	
	"	110 *	
	1740	200 *	
	"	230 *	
	1805	100	
	1900	150 *	
	2045	100 *	
	"	200 *	
	2345	200 * ✓	
2/25/79 99	0315	500 *	4.179
	0545	500 *	
	0815	450 *	
	0940	500 *	
	1020	500	
	1340	300 *	
	1430	200 *	
	1700	483 *	
	"	217 *	
	1830	115 *	
	1940	150 *	
	2058	150 *	
	2345	250 * ✓	

Not Found on Strip Chart

2400 END 14 days

Date	Time	water	% Power	
2/27/79	0000	start	97%	1420 - 200 gal
	0600	1000		2095 - 150
	0620	200		2245 - 103
	0900	200		59
	0955	150		
	1010	200		
	1150	200		
	1210	200		
	1225	200		
	1542	200		
	"	150		
	1603	200		
	1725	200		
	2/28/79	0000	start	98%
101	0016	200 *		
	0211	200 *		
	0251	410 *		
	0445	600 *		
	0730	200 *		
	0845	200 *		
	1507	200 *		
	1230	300 *		
	1325	300 *		
	1415	400 *		
	"	200 *		
	1720	107 *		
	1850	100 *		
	"	250 *		
	2005	100 *		
	2027	150 *		
	2158	200 *		
	2330	150 *		
3/1/79	0215	150		3.309
102	0250	150		
	0400	150		
	0445	150		
	0545	500		
	0735	200 cont		

Skip

ML

100

Lowered Power



Date	Time	water	of power
3/1/79 cont.	0805	150	98%
	0925	150	
	0951	150	
	missing on copy	150	
	1217	200	
	1245	200	
	1530	203	
	1630	200	
	1743	266	
	1955	150	
	2023	300	
3/2/79	0005	340	4.291
103	"	200	
	0255	300	
	0430	340	
	"	200	
	0705	150	
	0850	150	
	1000	400	
	1035	200	
	1305	200	
	1325	200	
	1600	250	
	1705	250	
	1850	250	
	2050	150	
	2140	250	
	2235	150	
	2330	450	
3/3/79	0230	250 *	3.791
104	"	240 *	
	0335	150 *	
	0522	150 *	
	0540	300 *	
	0745	150 *	
	0902	200 *	
	1040	300 *	
	1150	150 *	
	cont.		

Date	Time	Water	ab Power
3/3/99	1225	150 *	98%
	1335	150 *	
	1420	150 *	
	1505	150 *	
	1615	150 *	
	1700	287 *	
	1840	287 *	
	2030	150 *	
	2215	150 *	
	2355	400 *	
3/4/99	0130	200 *	4697
105	"	200 *	
	0240	238 *	
	0535	200 *	
	"	200 *	
	0650	186 *	
	0900	300 *	
	0950	200 *	
	1120	300 *	
	1438	200 *	
	1525	199 *	
	1659	395 *	
	1800	400 *	
	1840	- 462 *	
	1950	193 *	
	2055	300 *	
	2150	200 *	only 200
	2310	200 *	
	2345	200 *	
			end

Shut down
on 3/6
SU on 3/7

Date	Time	Water	No. Buses	
3/8/79	0000	Start	98%	4.614
106	0110	200 *		5.500
	0152	250 *		
	0403	228 *		
	0625	200 *		
	0830	250 *		
	0845	250 *		
	0903	200 *		
	0946	200 *		
	0950	100 *		
	0952	200 *		
	1024	200 *		
	1100	250 *		
	1250	400 *		
	1350	200 *		
	1535	200 *		
	1550	150 *		
	1650	200 *		
	1710	200 *		
	1730	200 *		
	1755	400 *		
	1930	300 *		
	1950	200 *		
	2030	250 *		
	2215	200 *		
	2320	250 *		
3/9/79	0045	255 *		5.410
107	0223	300 *		
	0315	150 *		
	0415	180 *		
	0540	250 *		
	0615	200 *		
	0910	586 *		
	"	14 *		
	1155	300 *		
	1230	600 *		
	1246	300 *		
	1420	300 *		
		cont		

Date	Time	Water	% Power
3/9/79 cont	1525	200 ✓	98%
107	1540	200 ✓	
	1730	200 ✓	
	1750	200 ✓	
	1850	250 ✓	
	2020	300 ✓	
	2135	300 ✓	
	2315	500 ✓	
3/10/79	0105	300 ✓	5.422
108	0230	400 ✓	
	0346	400 ✓	
	0500	300 ✓	
	0745	600 ✓	
	0746	100 ✓	
	0814	100 ✓	
	0852	200 ✓	
	0914	200 ✓	
	0921	200 ✓	
	0950	200 ✓	
	1115	600 ✓	
	1505	100 ✓	
	1555	200 ✓	
	1730	300 ✓	
	1845	300 ✓	
	1930	100 ✓	
	2015	250 ✓	
	2120	250 ✓	
	2230	250 ✓	5598
	2340	248 ✓	5598
3/11/79	0140 ⁰⁸⁴⁰	248 ✓	5.103
109	0150	250 ✓	
	0320	250 ✓	
	0500	20	
	"	(250) ^{Additional} continuous amt. entered. Feed & Bleed	
	0615	250 ✓	
	0728	510 ✓	
actually 2	"	90 ✓	
	0840	300 ✓	
		cont.	

Date	Term	Water	Power
3/11/79 109	0955	300 ✓	98%
	1200	300 ✓	
	1400	450 ✓	
	1500	300 ✓	
	1537	300 ✓	
	1711	300 ✓	
	1825	200 ✓	
	1850	200 ✓	
	2000	200 ✓	
	2100	150 ✓	
	2115	200 ✓	
	2223	200 ✓	
	3/12/79 110	0010	
0130		300 ✓	
0325		300 ✓	
0415		300 ✓	
0620		300 ✓	
0717		600 ✓	
0846		200 ✓	
0903		100 ✓	
1005		200 ✓	
1024		100 ✓	
1242		100 ✓	
1320		100 ✓	
1520		150 ✓	
1615		250 ✓	
1650		250 ✓	
1721		160 ✓	
1900		250 ✓	
1945	200 ✓		
2015	200 ✓		
2207	200 ✓		
2250	200 ✓		
3/13/79 111	0010	300 ✓	5.464
	0100	250 ✓	
	0315	251 ✓	
	0510	250 ✓	
	0545	250 ✓	

Date	Time	Water	Power
3/13/79 cont.	0745	427	98%
111	"	223	
	0910	200 200	
	0920	150	
	1040	240	
	1200	305	
	1220	250	
	1400	320	
	"	80	
	1510	200	
	1610	200	
	1715	200	
	1810	250	
	1915	200	
	2007	200	
	2050	200	
	2150	200	
	2230	200	
	2320	45	
	"	250	
3/14/79	0025	250	9.927
112	0109	230	
	0200	250	
	0333	250	
	0434	250	
	0530	250	
	0625	250	
	0745	300	
	0815	250	
	1020	200	
	"	589	
	1100	150	
	1230	300	
	1250	200	
	1510	200	
	1525	200	
	1545	200	
	1705	300	

cont.

Date	Time	Water	Power
3/14/79 cont. 112	1740	200 ✓	98%
	1925	300 ✓	
	1933	200 ✓	
	2040	200 ✓	
	2145	200 ✓	
	2200	200 ✓	
	2330	200 ✓	
3/15/79 113	0050	400 ✓	5.291
	0230	350 ✓	
	"	150 ✓	
	0435	350 ✓	
	0625	350 ✓	
	0848	400 ✓	
	1235	350 ✓	
	1400	300 ✓	
	1505	400 ✓	
	1630	300 ✓	
	1740	150 ✓	
	"	150 ✓	
	1900	150 ✓	
	"	450 ✓	
	2023	300 ✓	
	2115	300 ✓	
2213	200 ✓		
2340	207 ✓		
2350	206 ✓		
3/16/79 114	0050	300 ✓	5.945
	0155	300 ✓	
	0300	100 ✓	
	0330	300 ✓	
	0515	300 ✓	
	0540	300 ✓	
	0730	600 ✓	
	0835	200 ✓	
	0905	200 ✓	
	1025	200 ✓	
	1240	400 ✓	
	1345	200 ✓	
1431	125 ✓		
	Cont.		

Date	Time	Water	Power
3/16/79 cont.	114	1606	400 ✓ 98%
		1700	200 ✓
		1830	400 ✓
		1915	100 ✓
		1930	100 ✓
		2050	200 ✓
		2130	200 ✓
		2222	200 ✓
		2300	200 ✓
		2345	200 ✓
3/17/79	115	0010	200 ✓
		0010	200 ✓
		0150	400 ✓
		0230	200 ✓
		0323	200 ✓
		0405	300 ✓
		0510	200 ✓
		0550	200 ✓
		0635	200 ✓
		0826	800 ✓
		0845	350 ✓
		0920	250 ✓
		1210	425 ✓
		1245	250 ✓
		1330	250 ✓
		1415	250 ✓
		1637	500 ✓
		1743	353 ✓
		1845	144 ✓
		1900	500 ✓
		2100	300 ✓
		2130	300 ✓
		2240	300 ✓
		2315	300 ✓
3/18/79	116	0040	300 ✓
		0220	300 ✓
		0240	300 ✓
		0315	250 ✓
			cont.

7.140

6.667

Date	Time	Water	% Power
3/18/79 cont.	0345	450	✓
116	0505	207	✓
	0600	150	✓
	0625	200	✓
	0845	657	✓
	"	267	✓
	1000	200	✓
	1045	200	✓
	1300	196	✓
	"	406	✓
	1416	200	✓
	1534	200	✓
	1545	200	✓
	1626	200	✓
	1800	200	✓
	1900	600	✓
	2015	400	✓
	2145	200	✓
	2230	200	✓
	2301	200	✓
	2345	200	✓
3/19/79	0050	200	✓
117	0100	200	✓
	0157	200	✓
	0230	200	✓
	0315	200	✓
	0355	200	✓
	0450	200	✓
	0505	200	✓
	0615	200	✓
	0637	200	✓
	0800	600	✓
	0930	300	✓
	1035	200	✓
	1200	450	✓
	1425	200	✓
	1525	300	✓
	1620	400	✓

5.450

cont.

Date	Time	Water	% Power
3/19/79 cont.	1730	300 ✓	
117	1750	250 ✓	
	"	27 ✓	
	2035	150 ✓	
	2105	150 ✓	
	2247	159 ✓	
	2253	141 ✓	
	3/20/79	2202	200 ✓
118	0050	200 ✓	
	0120	300 ✓	
	0225	200 ✓	
	0245	150 ✓	
	0330	200 ✓	
	0455	200 ✓	
	0555	250 ✓	
	0640	200 ✓	
	0725	250 ✓	
	0750	250 ✓	
	0828	250 ✓	
	0925	250 ✓	
	0955	400 ✓	
	1020	250 ✓	
	1105	250 ✓	
	1220	300 ✓	
	1438	400 ✓	
	1545	252 ✓	
	1622	100 ✓	
	1623	400 ✓	
1805	400 ✓		
1855	100 ✓		
1900	300 ✓		
2044	200 ✓		
2138	200 ✓		
2210	200 ✓		
2252	200 ✓		

cont.

Date	Time	Water	Power
3/20/79 cont.	2305	400 ✓	7.471
3/21/79	0020	200 ✓	
119	0100	400 ✓	
	0126	200 ✓	
	0256	100 ✓	
	0329	200 ✓	
	0405	200 ✓	
	0417	100 ✓	
	0455	200 ✓	
	0605	200 ✓	
	"	50 ✓	
	0715	250 ✓	
	0802	250 ✓	
	0850	250 ✓	
	0930	250 ✓	
	1040	350 ✓	
	"	150 ✓	
	1245	250 ✓	
	1330	250 ✓	
	1400	250 ✓	
	1515	150 ✓	
1605	502 ✓		
1700	804 ✓		
1730	100 ✓		
1745	157 ✓		
1815	500 ✓		
1930	300 ✓		
2050	300 ✓		
2100	200 ✓		
2301	200 ✓		
2330	400 ✓		
3/22/79	0016	200 ✓	6.876
120	0055	200 ✓	
	0145	200 ✓	
	0211	200 ✓	
		cont.	

Date	Time	Water	Power	
3/22/29 cont.	0256	400 ✓		
120	0353	200 ✓		
	0432	200 ✓		
	0507	200 ✓		
	0522	200 ✓		
	0607	200 ✓		
	0755	489 ✓		
		10 ✓		
		1315	600 ✓	
		1410	400 ✓	
		1530	250 ✓	
		1635	250 ✓	
		1730	350 ✓	
		1835	350 ✓	
		1900	450 ✓	
		1925	250 ✓	
		2017	250 ✓	
		2140	450 ✓	
	2205	250 ✓		
	2305	300 ✓		
	2345	250 ✓		
3/23/29	0015	300 ✓	7.652	
121	0110	300 ✓		
	0220	300 ✓		
	0250	300 ✓		
	0325	300 ✓		
	0350	200 ✓		
	0435	300 ✓		
	0450	200 ✓		
	0525	250 ✓		
	0630	200 ✓		
	0740	250 ✓		
	0750	300 ✓		
	0900	300 ✓		
	1100	300 ✓		

cont.

Date	Time	Water	% Power
3/17/79 Cont.	1130	300 ✓	
12/18	1250	300 ✓	
	1423	400 ✓	
	1430	200 ✓	
	1532	500 ✓	
	1655	500 ✓	
	1800	500 ✓	
	1920	300 ✓	
	2030	300 ✓	
	2150	500 ✓	
	2305	300 ✓	
3/24/79	0010	500 ✓	8.475
122	0137	300 ✓	
	0150	200 ✓	
	0330	200 ✓	
	0352	200 ✓	
	0445	300 ✓	
	0535	100 ✓	
	0600	100 ✓	
	0630	50 ✓	
	0630	50 ✓	
	0735	600 ✓	
	0843	200 ✓	
	1001	200 ✓	
	1034	200 ✓	
	1225	400 ✓	
	1321	400 ✓	
	1525	750 ✓	
	1530	100 ✓	
	1650	300 ✓	
	1700	300 ✓	
	1845	600 ✓	unclear markover
	1915	300 ✓	
	1930	400 ✓	
	2227	250 ✓	

74-11

Should be applied to new systems.

Date	Time	Water	Power	
3/24/79	2055	250 ✓		
	2105	350 ✓		
	2222	450 ✓		
	122	100 ✓		
	2315	300 ✓		
	2350	300 ✓		
3/25/79	0325	300 ✓	6.012	
	0450	300 ✓		
	0500	300 ✓		
	123	0608		300 ✓
		0636		200 ✓
		0845		300 ✓
		1045		300 ✓
		1130		300 ✓
		1215		300 ✓
		1330		300 ✓
		1407		300 ✓
		1440		300 ✓
		1505		300 ✓
		1545		300 ✓
		1800		300 ✓
	1915	600 ✓		
	2115	600 ✓		
	2255	600 ✓		
3/26/79	0020	200 ✓	7.700	
	"	300 ✓		
	0110	300 ✓		
	1500	300 ✓		
	0145	200 ✓		
	0220	200 ✓		
	0305	300 ✓		
	0315	100 ✓		
	0325	350 ✓		
	"	200 ✓		
0540	200 ✓			
0610	200 ✓			

really 600

Feed and Bleed

Don't ever remember going out
in group 5

Date	Time	Water	Power
3/26/79	0645	200 ✓	
125	0800	200 ✓	
	0835	200 ✓	
	0900	200 ✓	
	1000	300 ✓	
	1118	300 ✓	
	1145	300 ✓	
	1240	300 ✓	
	1530	700 ✓	
	1730	700 ✓	
	1945	700 ✓	
	2130	700 ✓	
	2300	300 ✓	
	2315	300 ✓	
3/27/79	0005	300 ✓	7.264
125	0043	300 ✓	
	0130	300 ✓	
	0415	300 ✓	
	0523	450 ✓	
	0625	300 ✓	
	0705	300 ✓	
	0757	200 ✓	
	0840	300 ✓	
	0933	300 ✓	
	1035	350 ✓	
	1135	300 ✓	
	1215	300 ✓	
	1314	300 ✓	
	1410	400 ✓	
	1545	600 ✓	
	1725	600 ✓	
	1925	600 ✓	
	2210	300 ✓	
	2240	400 ✓	
	2315	300 ✓	

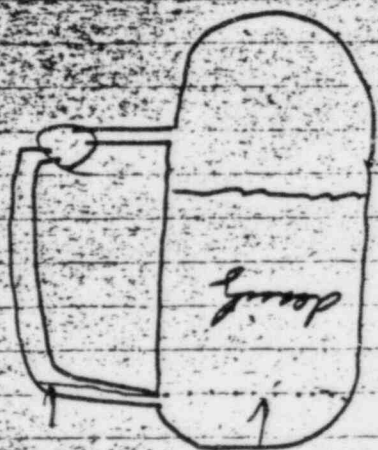
add 300 gal at 2300
20 drop

Linwood 2/12/04

11

1st = 1/2

= 12' 12'



GENERATION MAINTENANCE SYSTEM
MANUAL PERFORMANCE FORM

K-3

DATE ISSUED _____

SCHED. DATE _____

REFERENCE MANUAL _____

DEPT RESP - _____

TASK NO. - _____

WORK ORDER NO. - _____

ACCOUNT NO. - _____

GC CODE - _____

COMPONENT NO. - _____

COMPONENT DESC - _____

PLANT CONDITION (MODE) SU(2) OP(1) HD(4) CD(5) RF(6) HS(3) LR(1)

FREQUENCY _____ COMPONENT STATUS _____

SPECIFIC DAY _____ INTERFERENCE _____

PRIORITY _____

COMP. LOCATION - BDG _____ I.VL _____ GRID _____

PART NO QUAN SPEC EQUIPMENT

DEPENDENT TASKS ASSIST DEPT

SHIFT FOREMAN APPROVAL TO COMMENCE WORK

QC NOTIFIED BEFORE STARTING WORK (IF APPLICABLE ONLY)

COMPONENT RETURNED TO SERVICE (SHIFT FOREMAN)

SIGNATURE DATE RWP NO TAG NO

SIGNATURE DATE

SIGNATURE DATE

TXN. CD.	A.C.T.	COMPONENT NUMBER					LOCATION/UNIT	TYPE TASK	TASK IDENTIFICATION	SCHEDULE NUMBER		
		SYS	COMP. TYPE	COMP. ID.	LP	16				17	22	23-24
400	A	T	M	I	230130	1	03600	275	2301-301	7	9	0810

RESULTS (51) COMPLETE THIS SECTION (401A) DATE PERFORMED (39): 03 MONTH 22/1 DAY 17 19 YEAR

- CHECK ONE ONLY
- 1 PERFORMED OK
 - 2 EXCEPTIONS
 - 3 DEFICIENCIES
 - 4 BOTH E S AND D S
 - 5 NOT PERFORMED

ACTUAL MANHOURS (45)
ACTION TAKEN CODE (52)
REASON NOT PERFORMED (54)

10190010.15
L L I
L L I

PERFORMED BY EMPLOYEE NUMBER (60)

061504
0514551

SIGNATURE - _____

APPROVED BY EMPLOYEE NUMBER (65)

SIGNATURE - _____

WITNESSED BY EMPLOYEE NUMBER (70)

L L L L L I SIGNATURE - _____

CORRECTIVE MAINTENANCE JOB TICKET NUMBER (75) L L L L L I

403A (1) DUPLICATE AS ABOVE (5-38) 402 (1) DUPLICATE AS ABOVE (5-38)

RESULTS DESCRIPTION ASSISTING DEPARTMENTS

L01L I (39)
L I (61)

CODE (39) L L L L L L I
HOURS(44) L L L L L L I L I

404A (1) DUPLICATE AS ABOVE (5-38)

L01L I (39)
L I (61)

CODE (50) L L L L L L I
HOURS(55) L L L L L L I L I

rcl

DATE: 3/21/79
TIME: 1:14:33

REACTOR COOLA. LEAKAGE TEST
SP 2301-301

NOTE: IF OPERATOR ACTION DECREASES RCS VOLUME THE DATA ENTRY FOR THAT ACTION MUST BE ... YOU MUST ENTER DEC. PT. WITH LEAKAGE VALUE ...

DESIGNED INTERVAL (1-8 HOURS)

- 1 ENTER OPERATOR CAUSED CHANGES TO THE ROOT FROM DS 4 (2301-301)
- 0 ENTER OPERATOR CAUSED CHANGES FROM DS 4 (2301-301)
- 207. ENTER IDENTIFIED LEAKAGE FROM DS 3 (2301-301) (GPM)
- 0 ENTER PRIMARY TO SECONDARY OTS TOE LEAK (GPM)
- 0

TIME	TCA (F)	TIA (F)	TCD (F)	TIB (F)	TAVE (F)	PRZR LVL (IN)	MUTS LVL (IN)	RCDT LVL (INCHES)
1:14:56:	556.830	605.700	557.041	605.727	501.402	215.301	75.780	76.000
2:14:56:	556.041	605.555	557.430	605.510	501.201	225.100	71.462	79.440

GROSS LEAK RATE (<30 GPM): 6.0519 GPM

TOTAL IDENTIFIED RCS LEAK RATE (<10 GPM): 4.1833 GPM

NET UNIDENTIFIED LEAK RATE (<1 GPM): 1.8680 GPM

OPERATOR: *Earl O. Hernandez*

APPROVED: *C. Smith*

Collected - 0.22 GPM

"EVALUATION"

1001

Three Mile Island Nuclear Station

SIDE 2

1001-4

Nuclear Safety/Environmental Impact Evaluation

Procedure 2301-3D1

RCS Inventory

Temporary Change Notice No

Nuclear Safety Evaluation

Does the attached procedure change:

- * (a) increase the probability of occurrence or the consequences of an accident or malfunction of equipment important to safety? yes no
- * (b) create the possibility for an accident or malfunction of a different type than any evaluated previously in the safety analysis report? yes no
- * (c) reduce the margin of safety as defined in the basis for any technical specification? yes no

Details of Evaluation (Explain why answers to above questions are "no". Attach additional pages if required.)

Change now accurately takes into account RC leakage, collect and cooled in the RCDT. Change does not affect any operating conditions, and has no effect on nuclear safety.

Evaluation By J E Mork Date 3/16/79

3. Environmental Impact Evaluation

Does the attached procedure change:

- (a) possibly involve a significant environmental impact? yes no
(if 3(a) is "yes", answer questions (b) and (c) and fill in "Details of Evaluation" below.
If "no", state why by filling in the "Details of Evaluation" below) yes no
- * (b) have a significant adverse effect on the environment? yes no
- * (c) involve a significant environmental matter or question not previously reviewed and evaluated by the N.R.C. yes no

Details of Evaluation (Attach additional pages if required)

[Handwritten signature]

Evaluation By _____ Date _____

4. Unit Superintendent requests PORC review Check if YES.

5. Approval

Evaluation Accompanying PCR

[Signature] 3/16/79
Unit Superintendent Date

Evaluation Accompanying TCN

Approval _____
SRO Licensee Date

Reviewed _____
Member of Plant Staff Date

Approval _____
Unit Superintendent Date

11 The Evaluation "Accompanying a PCR" evaluation and approval chain may be followed at anytime.

NOTE: Instructions and guidelines in AP 1001 must be followed when completing this form.

TCN NO. 277

Unit No. 2

Date 3/16/79

1. Procedure 2301-3A1 RCS Inventory

2. Change (Include page numbers, paragraph numbers, and exact wording of change.)
see attached

3. Reason for Change:
To more accurately account for RCS leakage collected in the drain tank.

4. Recommended by JE Morck 3/16/79 5. JE Morck 3/16/79
(Date) (Date) Supervisor's Signature Date

6. Duration of TCN - No longer than ninety days from effective date of TCN or as in (a) or (b) below whichever occurs first.
(a) TCN will be cancelled by a procedure revision issued as a result of a Procedure Change Request to be submitted by MORCK (Submit PCR as soon as possible)
Supervisor Submitting TCN
(b) TCN is not valid after _____
(fill in circumstances which will result in TCN being cancelled)

7. (a) Is the procedure on the Nuclear Safety Related Procedure List? (Sec. AP 1001 - Appendix B)
If "Yes", complete Nuclear Safety Evaluation. (Side 2 of this Form) Yes No
(b) Is the procedure on the Environmental Impact Procedure List? (Sec. AP 1001 - Appendix B)
If "Yes", complete Environmental Evaluation. (Side 2 of this Form) Yes No
(c) Does the change effect the intent of the original procedure? Yes No

NOTE: If all answers are "no" the change may be approved by the Shift Supervisor. If question (c) is answered "yes", the change must be reviewed by the PORC and approval by the Station/Unit Superintendent prior to implementation. If the answer to question (c) is "no" the change may be approved by two members of the plant management staff at least one of whom holds a senior reactor operators license on the unit affected in accordance with paragraph 3.6.4.2 of AP 1001.

8. Review and Approval

Block (c) "yes"	Block (c) "no"
Approved <u>[Signature]</u> <u>3/16/79</u> Shift Supervisor/Foreman Date	Approved _____ SRO License Date
Reviewed <u>JE Morck</u> <u>3/16/79</u> Date	Reviewed _____ Member Plant Mrg. Staff Date
Members <u>[Signature]</u> <u>3/16/79</u> Date	Reviewed _____ Chairman of PORC Date
Of PORC <u>[Signature]</u> <u>3/16/79</u> Date	Approved _____ Unit Superintendent Date
Contacted <u>[Signature]</u> <u>3/16/79</u> Date	
Approved <u>[Signature]</u> <u>3/16/79</u> Unit Superintendent Date	

NOTE: The block (c) "Yes" review and approval chain may be followed at anytime.

9. Approval
Manager, Generation Quality Assurance _____ Date _____

NOTE: MGOA approval required only on certain Administrative Procedures listed in Enclosure 7 of AP 1001

10. TCN is Cancelled _____
Shift Supervisor/Shift Foreman Date

Attachment 1A

Note: This attachment is not valid if operator caused RCDT level changes would record RCDT temperature (from computer pit 1033) 1.5

Calculate density (in $\frac{lb}{ft^3}$) of water in RCDT. Use line A, an assumed pressure of 15 psia, and Table 1. Interpolate.

<u>50°F</u>	<u>0 psia</u> .016024	<u>500 psia</u> .015198
<u>100°F</u>	.016130	.016106

(Density $[\frac{lb}{ft^3}] = \frac{1}{v} [\frac{ft^3}{lb}]$) Density = 62.1

Calculate density of RC. Use average Tave and Figure 1. Density = 44.57

Convert identified leak rate, collected in RC drain tank, to equivalent RC gallons.

Ident Leak Rate 4.1939 (from print-out) $\times \frac{\text{Density of RCDT line RD } 62.1}{\text{Density of RCS line C } 44.57}$

RC equivalent Identified Leak Rate = 5.8294 gpm

Subtract Equivalent Identified Leak Rate from Total Leak Rate to get Unidentified.

Attachment 1A cont.

Total Leak Rate	6.619	
- Equiv. Ident Leak Rate	5.494	gpm 3.43
Net Unident Leak Rate	.2225	gpm 2.813
		gpm 1.116

Accept Criteria

- Total Leak Rate must be < 30 gpm.
- Total Identified Leak Rate must be < 10 gpm.
- Net Unidentified Leak Rate must be < 1 gpm.

CONTROL ROOM CONTROLLED COPY FILE COPY

1303-1.1
Revision 7
05/25/76

K-4

THREE MILE ISLAND NUCLEAR STATION
UNIT #1 SURVEILLANCE PROCEDURE 1303-1.1
REACTOR COOLANT SYSTEM LEAK RATE

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<p>Unit 1 Staff Recommends Approval</p> <p>Approval <u>N/A</u> Date _____ Cognizant Dept. Head</p>	<p>Unit 2 Staff Recommends Approval</p> <p>Approval _____ Date _____ Cognizant Dept. Head</p>
<p>Unit 1 PORC Recommends Approval</p> <p><u>C. J. Hartman</u> Date <u>5-24-76</u> VICE Chairman of PORC</p> <p>PORC comments of <u>N/A</u> included (date)</p> <p>By _____ Date _____</p>	<p>Unit 2 PORC Recommends Approval</p> <p>_____ Date _____ Chairman of PORC</p> <p>PORC comments of <u>N/A</u> included (date)</p> <p>By _____ Date _____</p>

Approval J. J. [Signature] Date 5-25-76
Station Superintendent/
Unit Superintendent

THREE MILE ISLAND NUCLEAR STATION
UNIT #1 SURVEILLANCE PROCEDURE 1303-1.1
RC SYSTEM LEAK RATE

Required Interval -

Daily, when RCS temperature > 525°F.

1.0 PURPOSE

To evaluate reactor coolant system leakage in accordance with Technical Specification Table 4.1-2 item 7.

2.0 PLANT STATUS

- 2.1 Reactor coolant system temperature is greater than 525°F.
- 2.2 The Make-Up Tank level is between 66" and 96".
- 2.3 The pressurizer level is greater than 200".
- 2.4 Reactor power, temperature and pressure are in a steady state condition. (i.e. initial and final conditions approximately the same.)

3.0 LIMITS AND PRECAUTIONS

- 3.1 Avoid addition and removal of water from the reactor coolant and Make-Up systems during this test. The following operations should not be conducted during this test:
 - a. Make-Up or chemical addition to the make-up system.
 - b. Sampling of the RCS or make-up system.
 - c. Venting or draining of the RCS or make-up system.
 - d. Changing purification demineralizers or make-up filters in service.
 - e. Boration or deboration.

- 3.2 The RCS and makeup system should be maintained in a steady state condition during this test. Changes in valve line-ups, coolers-in-service, pumps-in-service, etc. should be avoided.
- 3.3 For the most accurate determination of the RCS leak rate, the initial and final conditions of reactor power, RCS temperature, pressure and pressurizer level should be identical.
- 3.4 The same sources should be used when recording initial and final RCS temperature, pressurizer level, make-up tank level and RCDT level. Differences in sources could be misinterpreted as RCS leakage when comparing successive readings.
- 3.5 Minimize power level variations during this test.

4.0 LOCATION OF SYSTEM/ASSEMBLY

NOTE: See enclosure two for sources of data.

- 4.1 The computer is the favored source of information.
- 4.2 If two or more inputs are not obtainable on the computer, the patch panel is to be used to obtain the required data.

5.0 EQUIPMENT

- 5.1 Equipment for use on patch panel.
 - 5.1.1 Digital voltmeter capable of reading ± 10 VDC.
 - 5.1.2 Leads for patch panel to voltmeter.

6.0 PROCEDURE

- 6.1 If the computer is available, initiate the "Reactor Coolant Leakage Test" as detailed in Enclosure II. Data sheets for hand calculations are provided for use as follows:

Data Sheet

1303-1.1.1.1

For Use When

Computer is operational

but not available for
RCS program.

1303-1.1.1.2

Computer not operational

- 6.2 If a hand calculation is being performed, obtain the applicable data sheet (see step 6.1) and take the initial set of data. After a minimum of one hour, take the final set of data and determine the net RCS leak rate as per instructions on the data sheet.
- 6.3 If changes to the RCS inventory must be made during the performance of this test, they must be accounted for using Data Sheet 1303-1.1.3. Operations such as adding water to the Make Up Tank or sampling the RCS may be accounted for in this manner.
- 6.4 If the net RCS leakage is excessive as defined by the acceptance criteria in section 7, proceed as follows:
- 6.4.1 Perform another determination of the RCS leak rate.
- 6.4.2 Insure that no un-accounted for operator action has occurred that would change the RCS inventory. (See section 3.1 for a listing of possibilities). If such an action has occurred, it invalidates the measurement. Enter this in the "Remarks" section of the data sheet, clearly describing the action that invalidated the measurement.
- 6.4.3 Initiate action to determine the source of leakage. Check items such as:
- a. Proper valve line-up.

- b. Valve stem leakage.
- c. Make-up pump packing glands.
- d. Relief valves not seated properly.

6.4.4 If sources of leakage are found, initiate data sheet 1303-1.1.2.

- a. Document completely the source of leakage. (Example: MU-V-159A stem leakage through packing gland).
- b. Determine the leak rate. The most preferred method is to collect the leakage in a calibrated container. (Obtain from Chemistry Dept.) over a known period of time. Use data sheet 1303-1.1.2 to document the method used to determine the leak rate. Include: Model # & Serial # of DVM used, description of other equipment used, length of measurement and quantity of leakage collected (Example: Used 50 cc graduated cylinder to collect 40 cc of water in 10 seconds.)
- c. Determine the leak rate and enter on Data Sheet 1303-1.1.2.

This quantity may be subtracted from the net RCS leakage (Line 8C of Data Sheet 1303-1.1.1 and 1.1.2).

- d. The Shift Supervisor shall make the initial determination of the safety implications of the leak. If he decides that there are possible safety implications, he shall notify the proper personnel in accordance with AP 1014.

7.0 ACCEPTANCE CRITERIA

7.1 If the gross reactor coolant leakage rate (Item 7 of Data Sheet) exceeds 10 gpm, the reactor shall be placed in hot shutdown within 24 hours of detection.

- 7.2 If unidentified reactor coolant leakage (Item 9 of Data Sheet) exceeds 1 gpm of the reactor shall be placed in hot shutdown within 24 hours of detection.
- 7.3 If any reactor coolant leakage is evaluated as unsafe, the reactor shall be placed in hot shutdown within 24 hours of detection.
- 7.4 If any reactor coolant leakage exists through a non-isolable fault in a RCS strength boundary (such as the reactor vessel, piping, valve body, etc., except the steam generator tubes), the reactor shall be shutdown, and cooldown to the cold shutdown condition shall be initiated within 24 hours of detection.
- 7.5 If reactor shutdown is required by criteria 7.1, 7.2, 7.3, or 7.4, the rate of shutdown and the conditions of shutdown shall be determined by the safety evaluation for each case and justified in writing as soon thereafter as practicable.
- 7.6 Action to evaluate the safety implication of reactor coolant leakage shall be initiated within four hours of detection. The nature, as well as the magnitude, of the leak shall be considered in this evaluation. The safety evaluation shall assure that the exposure of offsite personnel to radiation is within the guidelines of 10 CFR 20.
- 7.7 If reactor shutdown is required per Specification 7.1, 7.2, 7.3, the reactor shall not be restarted until the leak is repaired or until the problem is otherwise corrected.
- 7.8 Loss of reactor coolant through reactor coolant pump seals and system valves to connecting systems which vent to the gas vent header and from which coolant can be returned to the reactor

coolant system shall not be considered as reactor coolant leakage and shall not be subject to the consideration of the above criteria except that such losses when added to leakage shall not exceed 30 gpm. If leakage plus losses exceeds 30 gpm the reactor shall be placed in hot shutdown within 24 hours of detection.

DATA SHEET 1303-1.1.1.1

For Use When Computer is Available

Initial Conditions - To be taken at one minute intervals

Line 1	Time	Computer Point	T ₁	T ₂	T ₃	T ₂ =
Line 2a	T _C Loop A	510	_____ + _____	_____ + _____	_____ = _____	+3= _____
Line 2b	T _H Loop A	508	_____ + _____	_____ + _____	_____ = _____	+3= _____
Line 2c	T _C Loop B	513	_____ + _____	_____ + _____	_____ = _____	+3= _____
Line 2d	T _H Loop B	509	_____ + _____	_____ + _____	_____ = _____	+3= _____
Line 2e	Unit Tave	(Sum of Lines 2a, 2b, 2c and 2d ÷ 4)				+4= _____
Line 3	Przr Level	1720	_____ + _____	_____ + _____	_____ = _____	+3= _____
Line 4	MU T _k Level	498	_____ + _____	_____ + _____	_____ = _____	+3= _____
Line 5	RCDT Level	Patch Panel DVM	_____ + _____	_____ + _____	_____ = _____	+3= _____

Final Conditions - To be taken at one minute Interyals

Line 6	Time	Computer Point	T ₁	T ₂	T ₃	T ₂ =
Line 7a	T _C Loop A	510	_____ + _____	_____ + _____	_____ = _____	+3= _____
Line 7b	T _H Loop A	508	_____ + _____	_____ + _____	_____ = _____	+3= _____
Line 7c	T _C Loop B	513	_____ + _____	_____ + _____	_____ = _____	+3= _____
Line 7d	T _H Loop B	509	_____ + _____	_____ + _____	_____ = _____	+3= _____
Line 7e	Unit Tave	(Sum of Lines 7a, 7b, 7c and 7d ÷ 4)				+4= _____
Line 8	Przr Level	1720	_____ + _____	_____ + _____	_____ = _____	+3= _____
Line 9	MU T _k Level	498	_____ + _____	_____ + _____	_____ = _____	+3= _____
Line 10	RCDT Level	Patch Panel DVM	_____ + _____	_____ + _____	_____ = _____	+3= _____

NOTE: Carry Algebraic signs through all steps.

1. Mass change due to RCS Temperature change.

(use line 2e and Figure 1 to determine density)

Line 11 a. Initial Density _____ lbm/ft³

(use line 7e and figure 1 to determine density)

Line 12 b. Final Density _____ lbm/ft³

- c. RCS Volume change (line 11 minus line 12 x 10,673)

Line 11 _____

Minus Line 12 _____

Line 13 10,673 ft³ x _____ lbm/ft³ = _____ lbm

2. Mass change in Pzrz. Level

(Line 3 minus Line 8 x 120.8)

Line 3 _____

Minus Line 8 _____

Line 14 120.8 $\frac{\text{lbm}}{\text{in}}$ x _____ in = _____ lbm

3. Mass change in MU Tank Level

(Line 4 minus Line 9 x 250 lbm/inch)

Line 4 _____

Minus Line 9 _____

Line 15 250 $\frac{\text{lbm}}{\text{in}}$ x _____ in = _____ lbm

4. Total RCS Mass Change

(Algebraic sum of lines 13, 14 and 15)

Line 13 _____ Total change of mass

Line 14 _____ Pressurizer mass change

Line 15 _____ MUT mass change

Line 16 _____ lbm

5. Total RCS change in gallons

- a. Mean Tave (line 2 plus line 7; + 2)

Line 2e ____ °F

+Line 7e ____ °F

Line 17 ____ + 2 = ____ °F

- b. Use figure 2 and Line 17 to find

Line 18 conversion factor from lbm to gallons: ____ gal/lbm

- c. RCS Inventory change (Line 16 times line 18)

Line 16 ____ lbm

Line 19 xLine 18 ____ gal/lbm = ____ gal

- d. Operator caused changes to system

Line 20 (from data sheet 1303-1.1.3): ____ gal

- e. Total RCS leakage plus losses

(Algebraic sum of lines 19 and 20)

Line 19 ____

Line 20 ____

Line 21 ____ gal.

6. Total leakage plus losses

- a. Duration of Test (Line 6 minus Line 1)

Line 6 ____ h ____ m

-Line 1 ____ h ____ m

Line 22 ____ h ____ m = ____ min

- b. Leak Rate (Line 21 divided by Line 22)

Line 21 ____

Line 23 +Line 22 ____ = ____ gpm

LIMIT: Line 23 shall not exceed 30 gpm (see acceptance criteria 7.8).

7. Gross Leak Rate

a. Mass change in RCDT

(Line 5 minus line 10 x 3540 lbm/volt)

Line 5 ____

-Line 10 ____

Line 24 ____ v x 3540 lbm/volt = ____ lbm

b. RCDT change in gallons

(Line 24 times Line 18)

Line 24 ____

xLine 18 ____ (Conversion factor)

Line 25 = ____ gal

c. Operator caused changes to the RCDT ____

Line 26 (from date sheet 1303-1.1.3): ____ gal

d. Gross RCS Leakage

(Algebraic sum of Lines 21, 25 and 26)

Line 21 ____ Total RCS Leakage + Losses

Line 25 ____ RCDT increase (considered RCS losses)

Line 26 ____ RCDT change by operator

Line 27 ____ gal

e. Gross RCS leak rate (identified and unidentified leakage)

(Line 27 divided by line 22)

Line 27 ____

Line 28 +Line 22 ____ = ____ gpm

LIMIT: Line 28 shall not exceed 10 gpm. (See Acceptance Criteria 7.1)

- 8. Corrections (identified leakage)
 - a. Evaporative losses -.51 gpm
 - b. RCPump Seal #3 Purge +.28 gpm
 - c. Identified leakage - _____ gpm (sign is minus)
(from data sheet 1303-1.1.2)

Line 29 Total (Algebraic sum) _____ gpm

- 9. Net unidentified RCS Leak Rate
Algebraic sum of lines 28 and 29

Line 28: _____

Line 29: _____

Line 30 _____ gpm

LIMIT: Line 30 may not exceed 1 gpm (See Acceptance
Criteria 7.2 and section 6.4 for action)

Remarks:

DVM Model # _____ Serial # _____

Performed by _____ Date _____

Approved by _____ Date _____

DATA SHEET 1303-1.1.1.2

For Use When Computer is Not Available

Initial Conditions - To be taken at one minute intervals

Line	Time	Patch Panel Point	T ₁	T ₂	T ₃	T ₂ =
Line 1	Tave	40	_____	_____	_____	_____
Line 2	Przr level	27	_____	_____	_____	+3=
Line 3	MU Tank	15	_____	_____	_____	+3=
Line 4	RCDT	DVM	_____	_____	_____	+3=

Final Conditions - To be taken at one minute intervals

Line	Time	Patch Panel Point	T ₁	T ₂	T ₃	T ₂ =
Line 6	Tave	40	_____	_____	_____	+3=
Line 7	Przr Level	27	_____	_____	_____	+3=
Line 8	MU Tank	15	_____	_____	_____	+3=
Line 9	RCDT	DVM	_____	_____	_____	+3=

Caution: When using patch panel voltage, be sure to record the voltage polarity (+ or -) and treat this as an algebraic sign.

NOTE: Carry Algebraic Signs Through all Steps

1. Volume change due to RCS temperature

a. Temperature conversions

1) Initial temperature (570 minus, line 2 times 5):

$$570^{\circ}\text{F} - (\text{Line } 2 \text{ } \underline{\hspace{1cm}} \times 5) = \underline{\hspace{1cm}}^{\circ}\text{F}$$

Line 11

2) Final temperature (570 minus line 7 times 5):

$$570^{\circ}\text{F} - (\text{Line } 7 \text{ } \underline{\hspace{1cm}} \times 5) = \underline{\hspace{1cm}}^{\circ}\text{F}$$

Line 12

b. Initial Density (use Line 11 and figure 1

Line 13 to determine density) $\underline{\hspace{1cm}}$ lbm/ft³

c. Final Density (use line 12 and figure 1

Line 14 to determine density) $\underline{\hspace{1cm}}$ lbm/ft³

d. RCS volume change (line 13 minus line 14, times 10,673)

Line 13 $\underline{\hspace{1cm}}$

-Line 14- $\underline{\hspace{1cm}}$

Line 15 10,673 ft³ x $\underline{\hspace{1cm}}$ = $\underline{\hspace{1cm}}$ lbm

2. Volume change in Pszr level

(Line 3 minus Line 8 x 120.8)

Line 3 $\underline{\hspace{1cm}}$

-Line 8- $\underline{\hspace{1cm}}$

Line 16 120.8 lbm/in x $\underline{\hspace{1cm}}$ in = $\underline{\hspace{1cm}}$ lbm

3. Volume change in MU Tank Level

(Line 4 minus line 9; times 250)

Line 4 $\underline{\hspace{1cm}}$

-Line 9- $\underline{\hspace{1cm}}$

Line 17 250 lbm/in x $\underline{\hspace{1cm}}$ in = $\underline{\hspace{1cm}}$ lbm

4. Total RCS Mass change
(Algebraic sum of lines 15, 16 and 17)

Line 15 _____ Tave change of mass

Line 16 _____ Pressurizer mass change

Line 17 _____ MUT mass change

Line 18 _____ lbm

5. Total RCS change in gallons

a. Mean Tave (Line 11 plus Line 12; + 2)

Line 11 _____ °F

+Line 12 _____ °F

Line 19 _____ + 2 = _____ °F

b. Use figure 2 and line 19 to find

Line 20 conversion factor from lbm to gallons: _____ gal/lbm

c. RCS Inventory change (line 18 times line 20)

Line 18 _____ lbm

Line 21 xLine 20 _____ gal/lbm = _____ gal

d. Operator caused changes to system

Line 22 (from data sheet 1303-1.1.3): _____ gal

e. Total RCS leakage plus losses

(Algebraic sum of lines 21 and 22)

Line 21 _____

+line 22 _____

Line 23 _____ gal.

6. Total leakage plus losses

a. Duration of test (line 6 minus line 1)

Line 6 _____ h _____ m

-Line 1 _____ h _____ m

Line 24 _____ h _____ m = _____ min

b. Leak rate (line 23 divided by line 24)

Line 23 _____

Line 25 +Line 24 _____ = _____ gpm

LIMIT: Line 25 shall not exceed 30 gpm (see Acceptance
Criteria 7.8)

7. Gross leak rate

a. Mass change in RCDT

(Line 5 minus line 10 x 3540 lbm/volt)

Line 5 _____

-Line 10 _____

Line 26 _____ v x 3540 lbm/volt = _____ lbm

b. RCDT change in gallons

(Line 26 times line 20)

Line 26 _____

xLine 20 _____ (Conversion factor)

Line 27 = _____ gal

c. Operator caused changes to the RCDT

Line 28 (from data sheet 1303-1.1.3): _____ gal

d. Gross RCS leakage

(Algebraic sum of lines 23, 27 and 28)

Line 23 _____ Total RCS leakage + losses

Line 27 _____ RCDT increase (considered RCS losses)

Line 28 _____ RCDT change (by operator)

Line 29 _____ gal

e. Gross RCS leak rate (identified and unidentified leakage)

(line 29 divided by line 24)

Line 29 _____

Line 30 +Line 24 _____ = _____ gpm

LIMIT: Line 30 shall not exceed 10 gpm. (see
Acceptance Criteria 7.1)

- 8. Corrections (identified leakage)
 - a. Evaporative losses -.51 gpm
 - b. RCPump Seal #3 Purge +.28 gpm
 - c. Identified Leakage - _____ gpm (sign is negative)
(from data sheet 1303-1.1.2)

Line 31 Total (Algebraic sum) _____ gpm

- 9. Net unidentified RCS Leak Rate
(Algebraic sum of lines 30 and 31)

Line 30 _____

Line 31 _____

Line 32 _____ gpm

LIMIT: Line 32 may not exceed 1 gpm. (See Acceptance
Criteria 7.2 and section 6.4 for action)

Remarks:

DVM Model # _____ Serial # _____

Performed by _____ Date _____

Approved by _____ Date _____

Data Sheet 1303-1.1.2

IDENTIFIED LEAKAGE

1. Source of Leakage
(Describe in detail, attach drawings if necessary)

2. Method used to determine leak rate
(Describe briefly)

3. Leak Rate: _____ gpm
(For use in step 8.c of Data Sheet 1303.1.1.1.1 and 1.1.1.2)

_____ Performed By _____ Date _____

4. Possible Safety Implications
(Shift Supervisor Check One)

_____ Yes (Initiate necessary action)

_____ No Explain _____

_____ Shift Supervisor _____ Date _____

Data Sheet 1303-1.1.3

OPERATOR CAUSED CHANGES TO RCS INVENTORY

1. Identify operation that caused change: _____

2. Time Operation Started: _____
Time Operation Completed: _____

3. Calculations

4. Total change to RCS inventory: _____ gal.

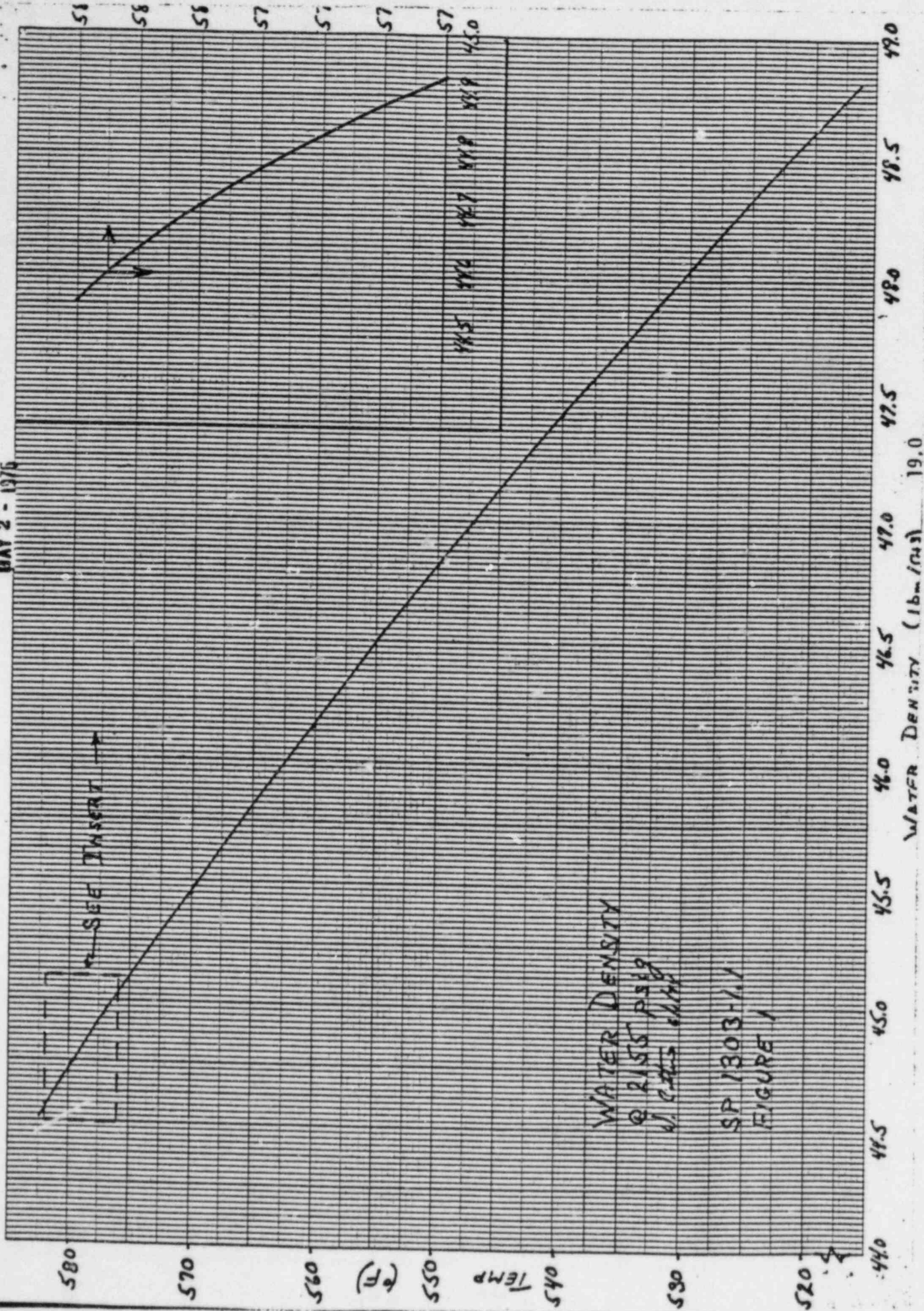
- NOTES: 1) If change is to RCDT enter in section 7 of Data Sheet 1303-1.1.1.1 and 1303-1.1.1.2
- 2) If change is to any other part of the system, enter in section 5 of Data Sheet 1303-1.1.1.1 or 1.1.1.2
- 3) SIGNS: Removals from the system have a negative (-) sign. Additions to the system have a positive (+) sign.

Performed By Date

Approved By Date

1303-1.1

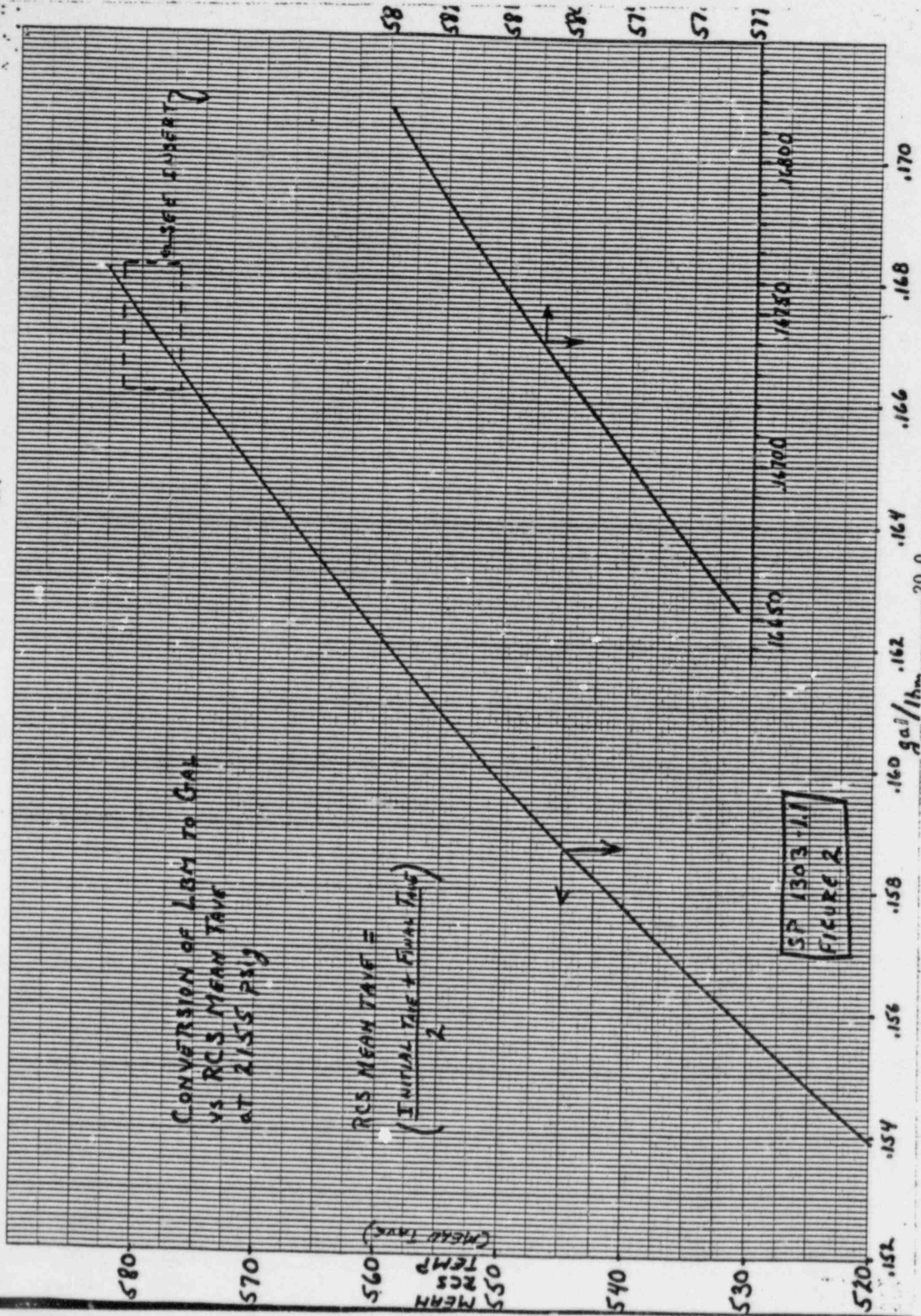
Revision 4
MAY 2 - 1976



WATER DENSITY
@ 2155 PSIG
V. C. 2155 6/11/76

SP 1303-1.1
FIGURE 1

1303-1.1



ENCLOSURE I
SOURCES OF DATA

PARAMETER	COMPUTER POINT	CONTROL ROOM INSTRUMENTATION	PATCH PANEL			
			POINT	RANGE	(VDC) OUTPUT	MULTIPLIER
Tave	508 Loop A T _c	RC 7-TAR or RC 8-T 1	40 (unit Tav)	520-620 ^o F	+10 to -10	T=570-(5xvolts)
	510					
	511 Loop A T _H					
	512					
	509 Loop B T _c					
	513					
	514 Loop B T _H					
515						
Pressurizer Level	1720	Control Console Center Panel	27	0-400 in	+10 to -10	4000 lbm/volt
	1721					
	1722					
Make-up Tank Level	458	Control Console Center Panel	15	0-100 in	-10 to +10	-1250 lbm/volt
Reactor Coolant Drain Tank Level	DVM at Patch Panel	Level Recorder LWDS Panel	71	0-120 in	0-to +10	3540 lbm/volt

Note: Patch Panel Data may be obtained from the voltmeters installed for a cooldown from outside the Control Room

ENCLOSURE II

Computer Determination of RC
Leak Rate

E.2.1.0 PURPOSE

This program is designed to perform all the calculations accomplished on Data Sheet 1303-1.1.1.1. The plant computer will automatically gather all inputs and average three minute intervals of the initial and final readings. This program is run from the programmer's console of the Bailey 855 computer. It may be run at any time the programmer's console is not being used by another program.

E.2.2.0 PROCEDURE

E.2.2.1 Turn on the programmer's selectric typewriter next to the Bailey 855 computer. Be sure that the "OUTPUT SELECT" switch is on "UTILITY COMPUTER."

E.2.2.2.1 If the computer printout on the selectric shows a question mark (?), type "r", then depress the "Return" Key. The computer will respond with an exclamation mark (!). Proceed to E.2.2.2.2.

E.2.2.2.2 If the printout on the selectric shows an exclamation mark (!), type "RC" and then press the "Return" key. (See sample printout: Attachment 1)

E.2.2.3 The computer will then request the time interval over which the test is to be run. Any interval from 1 to 8 hours in one hour intervals may be chosen. Enter a single digit, then press the "Return" Key.

E.2.2.4 The computer will now request known leakage. Enter "Identified Leakage" (as determined by Data Sheet 1303-1.1.2) in gallons per minute. Enter operator caused changes to the RCDT or the RCS (as detailed on Data Sheet 1303-1.1.3) in gallons.

CAUTION: For the above entries, be sure to enter a decimal point. If no decimal point is entered, the computer will insert one according to the format it expects to see.

E.2.2.5 The computer will now print out all required data. Be sure to attach data sheets detailing any entries made in step E.2.2.4.

ATTACHMENT 1

!rc

DATE: 01/20/75
TIME: 16: 3:38

REACTOR COOLANT LEAKAGE TEST
SP 1303-1.1

DESIRED INTERVAL (1-8 HOURS)

1

ENTER IDENTIFIED LEAKAGE FROM DS 1303-1.1.2 (GPM)

ENTER RCDT CHANGE (GAL)

ENTER RCS CHANGE (GAL)

TIME	TCA (F)	THA (F)	TCB (F)	THB (F)	TAVE (F)	PRZR LVL (IN)	MUTK LVL (IN)	RCDT LVL (VOLT)
16: 3:54	556.977	601.055	556.250	600.719	578.750	238.311	79.603	8.925
16: 8:54	557.031	601.070	556.180	600.719	578.742	230.178	79.095	8.945

LEAKAGE PLUS LOSSES (<30 GPM): 0.0473 GPM

GROSS RCS LEAK RATE (<10 GPM): -0.1463 GPM

NET UNIDENTIFIED LEAK RATE (<1 GPM) -0.3763 GPM

OPERATOR:

APPROVED:

K-5

Calculator printer strip copies
with program and data from snwp
leak rate calculations done in 1980

000 91 R/S
 001 99 PRT
 002 91 R/S
 003 99 PRT
 004 98 ADV
 005 91 R/S
 006 42 STD
 007 11 11
 008 99 PRT
 009 75 -
 010 91 R/S
 011 42 STD
 012 12 12
 013 99 PRT
 014 95 =
 015 65 X
 016 43 RCL
 017 01 01
 018 65 X
 019 43 RCL
 020 02 02
 021 95 =
 022 42 STD
 023 10 10
 024 99 PRT
 025 98 ADV
 026 91 R/S
 027 99 PRT
 028 42 STD
 029 21 21
 030 75 -
 031 91 R/S
 032 99 PRT
 033 42 STD
 034 22 22
 035 95 =
 036 65 X
 037 43 RCL
 038 03 03
 039 65 X
 040 43 RCL
 041 04 04
 042 95 =
 043 44 SUM
 044 10 10
 045 99 PRT
 046 98 ADV
 047 91 R/S
 048 99 PRT
 049 42 STD
 050 31 31
 051 75 -
 052 91 R/S
 053 99 PRT
 054 42 STD
 055 32 32
 056 95 =
 057 65 X
 058 43 RCL
 059 03 05

060 95 =
 061 44 SUM
 062 10 10
 063 99 PRT
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 065 43 RCL
 066 10 10
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 068 55 +
 069 43 RCL
 070 06 06
 071 65 X
 072 43 RCL
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 072 91 R/S
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 078 02 2

079	00	0	140	65	x	201	13	13
080	02	2	141	43	RCL	202	43	RCL
081	99	PRT	142	20	20	203	01	01
082	91	R/S	143	85	+	204	55	+
083	76	LBL	144	43	RCL	205	01	1
084	13	C	145	11	11	206	00	0
085	99	PRT	146	65	x	207	00	0
086	42	STO	147	43	RCL	208	75	-
087	07	07	148	21	21	209	43	RCL
088	02	2	149	95	=	210	13	13
089	00	0	150	42	STO	211	95	=
090	03	3	151	12	12	212	65	x
091	99	PRT	152	43	RCL	213	01	1
092	91	R/S	153	06	06	214	00	0
093	76	LBL	154	55	+	215	00	0
094	14	D	155	01	1	216	85	+
095	99	PRT	156	00	0	217	06	6
096	42	STO	157	00	0	218	00	0
097	08	08	158	95	=	219	65	x
098	02	2	159	59	INT	220	43	RCL
099	00	0	160	42	STO	221	13	13
100	04	4	161	13	13	222	95	=
101	99	PRT	162	43	RCL	223	94	+/-
102	91	R/S	163	06	06	224	85	+
103	76	LBL	164	55	+	225	43	RCL
104	15	E	165	01	1	226	14	14
105	99	PRT	166	00	0	227	95	=
106	42	STO	167	00	0	228	35	1/X
107	09	09	168	95	=	229	65	x
108	02	2	169	75	-	230	43	RCL
109	00	0	170	43	RCL	231	12	12
110	05	5	171	13	13	232	95	=
111	99	PRT	172	95	=	233	99	PRT
112	98	ADV	173	65	x	234	98	ADV
113	43	RCL	174	01	1	235	98	ADV
114	00	00	175	00	0	236	43	RCL
115	99	PRT	176	00	0	237	06	06
116	43	RCL	177	85	+	238	42	STO
117	05	05	178	06	6	239	01	01
118	42	STO	179	00	0	240	43	RCL
119	00	00	180	65	x	241	07	07
120	43	RCL	181	43	RCL	242	42	STO
121	07	07	182	13	13	243	02	02
122	75	-	183	85	+	244	43	RCL
123	43	RCL	184	02	2	245	08	08
124	02	02	185	04	4	246	42	STO
125	95	=	186	65	x	247	03	03
126	99	PRT	187	06	6	248	43	RCL
127	42	STO	188	00	0	249	08	08
128	10	10	189	95	=	250	42	STO
129	43	RCL	190	42	STO	251	04	04
130	08	08	191	14	14	252	43	RCL
131	85	+	192	43	RCL	253	09	09
132	43	RCL	193	01	01	254	42	STO
133	04	04	194	55	+	255	04	04
134	95	=	195	01	1	256	91	R/S
135	99	PRT	196	00	0	257	00	0
136	42	STO	197	00	0	258	00	0
137	11	11	198	95	=	259	00	0
138	43	RCL	199	59	INT	260	00	0
139	10	10	200	42	STO	261	00	0

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263 00 0
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Page 3

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*LEAK
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*NO TO REPAIR
LEAKS
FOR
JUST
BODY
TO
GANNET
ISOL
VALVES*

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DATA MISSING

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201.
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-202.
3.186
203.
1.
204.
3.
205.

2479.
0.436
4.
1.107360428

201.
600.
202.
2.5
203.
2.
204.
3.
205.

32579.
-0.686
5.
.9158985265

201.
532.
202.
2.696
203.
3.
204.
4.
205.

32679.
0.196
6.
1.420081542

201.
-601.
202.
2.2
203.
0.
204.
0.
205.

32779.
-0.496
4.
1.555756785



DATA SHEET 1

2301-3D1
Revision 0
08/19/77

RCS LEAK RATE

For Use When Computer is Available

Initial Conditions - To be taken at one minute intervals

	Computer Point	t ₁	t ₂	t ₃		
Line 1	Time	1815	1816	1817	t ₂ = 1816	
Line 2a	T _C Loop A	394 393	326	325.9	325.9	= 977.8 ÷ 3 = 325.9 °F T _{CA}
Line 2b	T _H Loop A	390	+ assume same as T _C		+ 3 = °F T _{HA}	
Line 2c	T _C Loop B	397 396	325.1	325.1	325.1	= 975.2 ÷ 3 = 325.06 °F T _{CB}
Line 2d	T _H Loop B	391	+ assume same as T _C		+ 3 = °F T _{HB}	
Line 2e	Unit Tave	(Sum of Lines 2a, 2b, 2c, and 2d ÷ 4)			2 = 325.48 °F Tave	
Line 3	Przr Level	1682	123.9	123.9	124	= 371.8 ÷ 3 = 123.93 in L _{PZR}
Line 4	MU T _k Level	347	71.3	71.8	71.2	= 214.3 ÷ 3 = 71.43 in L _{MUT}
Line 5	RCDT Level	(Patch Panel DVM #64)	1.88	1.88	1.88	= 5.64 ÷ 3 = 1.88 V L _{RCDT}
	RC Pressure		1250 + 1250 + 1250 = 3750 ÷ 3 = 1250 psig.			

Final Conditions - To be taken at one minute intervals.

	Computer Point	t ₁	t ₂	t ₃		
Line 6	Time	1915	1916	1917	t ₂ = 1916	
Line 7a	T _C Loop A	394 393	325.9	325.9	326	= 977.8 ÷ 3 = 325.9 °F T _{CA}
Line 7b	T _H Loop A	390	+ assume same as T _C		+ 3 = °F T _{HA}	
Line 7c	T _C Loop B	397 396	325.1	325	325	= 975.1 ÷ 3 = 325 °F T _{CB}
Line 7d	T _H Loop B	391	+ assume same as T _C		+ 3 = °F T _{HB}	
Line 7e	Unit Tave	(Sum of Lines 7a, 7b, 7c, and 7d ÷ 4)			650.9 ÷ 4 = 325.45 °F Tave	
Line 8	Przr Level	1682	124.2	124.5	124.2	= 372.9 ÷ 3 = 124.3 in L _{PZR}
Line 9	MU T _k Level	347	69.2	68.7	68.5	= 206.4 ÷ 3 = 68.8 in L _{MUT}
Line 10	RCDT Level	(Patch Panel DVM #64)	2.02	2.02	2.02	= 6.06 ÷ 3 = 2.02 V L _{RCDT}
	RC Pressure		1250 + 1250 + 1250 = 3750 ÷ 3 = 1250 psig. 6.0			

DATA SHEET 1 (cont'd)

NOTE: Carry Algebraic signs through all steps.

1. Mass change due to RCS Temperature change.

(Use line 2e and ^{Steam Tables} Figure 1 to determine density)

Line 11

a. Initial Density 56.7281 lbm/ft³

(Use line 7^e and ^{Steam Tables} Figure 1 to determine density)

Line 12

b. Final Density 56.7291 lbm/ft³

c. RCS Volume change (line 11 minus line 12 x 10,678*
ft³)

SEE Additional
Calculations *

①

*NOTE: 10,678 ft³ is the RCS Volume for 582°F
minus the pressurizer. For 532°F use
10,673 ft³. If more accuracy is required
for other temperature >525°F use a linearly
extrapolated volume. 325°F = 10,645

②

Line 11 56.7281 lbm/ft³

-Line 12 56.7291 lbm/ft³

Line 13

~~10,678*~~ ^{10,645} ft³ x -0.0010 lbm/ft³ = -10.64 lbm

2. Mass change in Pzrz. Level

(Line 3 minus Line 8 x 120.8 lbm/in)

Line 3 123.93 in

-Line 8- 124.3 in

Line 14

^{142.2 lbm}
~~120.8~~ in x -0.37 in = -52.6 lbm

3. Mass change in MU Tank Level

(Line 4 minus Line 9 x 255 lbm/inch)

Line 4 71.43 in

-Line 9 68.8 in

Line 15

255 ^{lbm}/_{in} x 2.63 in = 670.65 lbm

③

DATA SHEET 1 (cont'd)

4. Total RCS Mass Change

(Algebraic sum of lines 13, 14, and 15)

Line 13 -10.64 RCS Tave change of mass

Line 14 -52.6 Pressurizer mass change

Line 15 670.6 MUT mass change

Line 15

RCS 607.36 Δlbm

5. Total RCS change in gallons

a. Mean Tave (line 2e plus line 7e + 2)

Line 2e 325.48 °F

+Line 7e 325.45 °F

Line 17

RCS 650.93 + 2 = 325.46 °F T_{MEAN}

b. Use Figure 2 and Line 17 to find

Line 18

Conversion factor from lbm to gallons: 0.131865 gal/lbm

c. RCS Inventory change (Line 16 times line 18)

Line 16 607.36 lbm

Line 19

xLine 18 0.131865 gal/lbm = 80.09 gal = RCS Volume Change

d. Operator caused changes to system

Line 20

(From Data Sheet 4): 0 gal

e. Total RCS Leakage

(Algebraic sum of lines 19 and 20)

Line 19 80.09 gal.

+Line 20 0 gal.

Line 21

RCS = 80.09 gal. Total Leakage

DATA SHEET 1 (cont'd)

6. Total Leak Rate

a. Duration of Test (Line 6 minus Line 1)

Line 6 .19 h 16 m

-Line 1 18 h 16 m

Line 2

= 1 h 0 m = 60 min

b. Leak Rate (Line 21 divided by Line 22)

Line 21 80.09 ÷ 60

Line 2

+Line 22 1,335 = gpm Total Leak Rate
(Identified and Unidentified)

7. Identified Leak Rate

a. Volume change in RCDT

(Use Figure 3 for level to volume conversion)

Line 5 1.88 V = 6,504 gal

-Line 10 2.02 V = 6,531 gal

Line 2

RCDT Volume Change = -27 gal

b. Operator caused change to the RCDT

Line 2

(From Data Sheet 4: 0 gal

CAUTION: Removing water from the RCDT

should be entered as a negative
change to the water inventory.

Line 2

c. Identified leakage: 0 gpm (sign should be minus) |
(From Data Sheet 3)

Line 2

d. Primary to Secondary OTSG Tube Leak: 0 gpm (Sign should
be minus) |

e. Identified Leakage to RC Drain Tank.

(Algebraic sum of Line 24, and 25).

05/04/78

Line 24 -27 RCDT Volume change

Line 25 0 RCDT change by operator

Line 28

-27 gal Identified RCS Leakage to RCDT

F. Identified Leak Rate to RCDT

Line 28 -27 gal.

Line 29

+ Line 22 60 m = -0.452 gpm Identified Leak Rate to RCDT (should be negative or zero)

g. Total Identified Leak Rate

(Sum of line 26, 27 and line 29)

Line 26 0 gpm Identified leakage (From Data Sheet 3)

Line 27 0 gpm Primary to Secondary leakage

+ Line 29 -0.452 gpm Identified Leak Rate to RCDT

Line 30

-0.452 gpm total.

Line 31

Abs value of line 30 0.452 gpm total Identified Leakage.

LIMIT: Line 31 shall not exceed 10 gpm. (See Acceptance Criteria 7.1)

Line 27 shall not exceed 1 gpm (See Acceptance Criteria 7.5)

8. Unidentified RCS Leak Rate

(Subtract Line 31 from Line 23)

Line 23 1.335 gpm Total Leak Rate

-Line 31 0.452 gpm Identified Leak Rate

Line 32

0.883 gpm Unidentified Leak Rate (1 gpm maximum)

LIMIT: Line 32 shall not exceed 1 gpm (See Acceptance Criteria 7.2).

REMARKS: Leakage within acceptable limits.

PERFORMED BY

J E Morck

APPROVED BY

B Mehler

DATE 12/19/78

DATE 12-19-78

Data from 12/18/78 @ 1815

2301-3D1

Additional Calculations.

To interpolate from steam tables for 325° RC:

<u>°F</u>	<u>1,000</u>	<u>1265</u>	<u>1500</u>	<u>f</u>
300	.017379	.0173599	.017343	
325.45 (final)		.0176276		56.72911
325.48 (initial)		.0176279		56.7281
350	.017909	.017885	.017865	

② To calculate RC Volume at low temperature.

<u>From 2101-1.1</u>		<u>From 2301-3D1</u>	
<u>TEMP</u>	<u>Vol (incl press)</u>	<u>Vol w/o pressurizer</u>	
582	11,477.5	10,678	∴ 800 gal in pressurizer.
532	11,473.1	10,673	
325		10,645 gal.	interpolate
140	11,420	10,620	
70	11,413	10,613.	

③ Pressurizer @ saturation temp @ 1250 psig = 1265 psia.

	<u>VF</u>	
1250	.02250	
		1265 = .022557 or f = 44.332.
1300	.02269	

$$24 \text{ gal/in} \times .13368 \frac{\text{ft}^3}{\text{gal}} \times 44.332 \frac{\text{lb}}{\text{ft}^3} = 1422 \text{ lbm/in.}$$

Calc. gal/lbm for RCS.

$$f = (56.7291 + 56.7281) \div 2 = 56.7286 \text{ } \frac{\text{lb}}{\text{ft}^3}$$

$$7.4805 \frac{\text{gal}}{\text{ft}^3} \div 56.7286 \frac{\text{lb}}{\text{ft}^3} = .131865 \text{ gal/lbm.}$$

⑤ RCDT interpolation

<u>VDC</u>	<u>GAL</u>
1.6	6.45×10^3
1.88	6.504×10^3
2.02	6.531×10^3
2.4	6.605×10^3

K-7

TEST NO. NOW 15 = 0001
 TEST NO. DESIRED 14 = 0001
 BLOCK NO. NOW 15 = 0001
 BLOCK NO. DESIRED 14 = 0001
 STARTING RECORD NO. 15 = 00750
 STARTING DATA SET NO. 12 = 01
 DECODING INTERVAL 15 = 00001
 PLAYBACK CHANNELS 12 =

01-02-03-04-05-06-07-08-09-10-11-12-99

TMI-2

Run Type NS C104, DATA AT 0400 gm 03-28-77

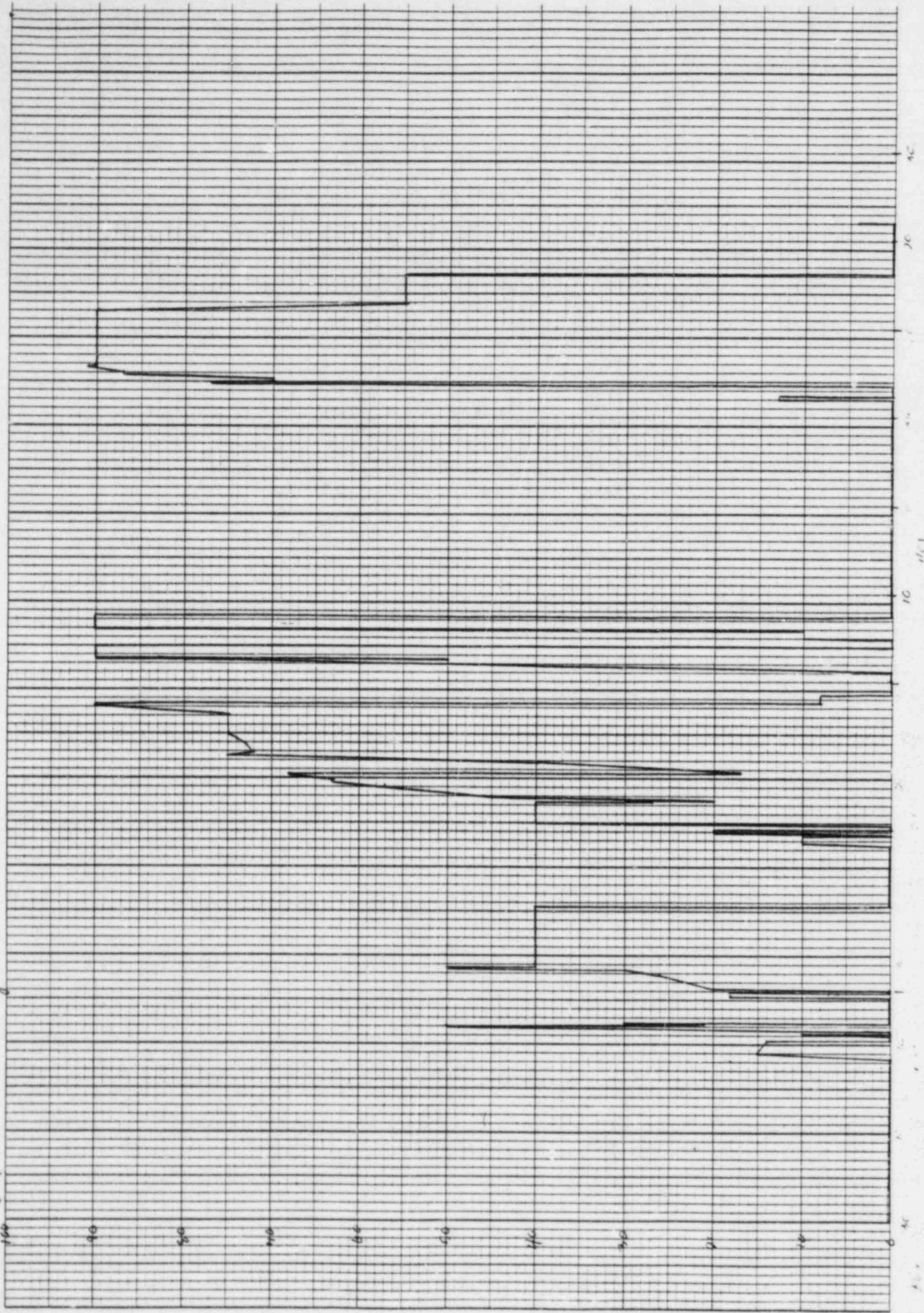
3rd RUNWAY, BRN TRIP AT RECORD 0760

DATA is from 70 and 30 minutes before Trip

*SWITCH 0 IS QUIET SWITCH *	(P)	T ₁ (OUT) (μs)	T ₂ (OUT) (μs)	T ₃ (OUT) (μs)	T ₄ (μs) (°F)	T ₅ (μs) (°F)	T ₆ (μs) (°F)	RES. USA (MPP)	RES. PAR Level (Coulombs)	ASS. AMT Level (Ends)	RES. USA (MPP)	RES. PAR Level (Coulombs)	ASS. AMT Level (Ends)	RES. USA (MPP)	RES. PAR Level (Coulombs)	ASS. AMT Level (Ends)	RES. USA (MPP)	RES. PAR Level (Coulombs)	ASS. AMT Level (Ends)	RES. USA (MPP)	RES. PAR Level (Coulombs)	ASS. AMT Level (Ends)	RES. USA (MPP)	RES. PAR Level (Coulombs)	ASS. AMT Level (Ends)
0000750	3	+0097.4	+0606.1	+0606.1	+0559.8	+0556.3	+0647.1	+0220.5	+0077.7	+0010.0	+0003.1	+2151.3	+0010.0												
0000750	3	+0097.5	+0606.0	+0606.2	+0559.8	+0556.3	+0647.3	+0220.7	+0077.7	+0010.0	+0003.1	+2151.5	+0010.0												
0000750	3	+0097.4	+0606.1	+0606.1	+0559.6	+0556.4	+0647.7	+0220.6	+0077.7	+0010.0	+0003.3	+2151.1	+0010.0												
0000750	3	+0097.4	+0606.1	+0606.1	+0559.7	+0556.4	+0647.1	+0220.9	+0077.7	+0010.0	+0002.9	+2151.3	+0010.0												
0000750	3	+0097.4	+0606.1	+0606.2	+0559.9	+0556.4	+0646.7	+0220.8	+0077.7	+0010.0	+0003.5	+2151.9	+0010.0												
0000750	3	+0097.4	+0606.1	+0606.3	+0559.9	+0556.5	+0647.5	+0221.0	+0077.8	+0010.0	+0003.4	+2151.7	+0010.0												
0000750	3	+0097.4	+0606.1	+0606.2	+0559.7	+0556.6	+0647.0	+0221.1	+0077.8	+0010.0	+0003.3	+2151.9	+0010.0												
0000750	3	+0097.4	+0606.1	+0606.4	+0559.8	+0556.7	+0647.9	+0221.0	+0077.8	+0010.0	+0003.5	+2151.5	+0010.0												
0000750	3	+0097.4	+0606.1	+0606.4	+0559.7	+0556.9	+0646.8	+0221.1	+0077.9	+0010.0	+0003.1	+2152.5	+0010.0												
0000750	3	+0097.5	+0606.1	+0606.3	+0559.9	+0556.8	+0647.1	+0221.2	+0077.9	+0010.0	+0003.5	+2151.5	+0010.0												
0000750	3	+0097.5	+0606.1	+0606.3	+0559.9	+0556.9	+0666.5	+0221.5	+0078.0	+0010.0	+0003.1	+2153.9	+0010.0												
0000750	3	+0097.5	+0606.2	+0606.5	+0560.0	+0557.1	+0034.9	+0221.6	+0078.0	+0010.0	+0003.5	+2152.3	+0010.0												
0000750	3	+0097.5	+0606.2	+0606.4	+0560.2	+0556.9	+0667.0	+0221.5	+0078.0	+0010.0	+0003.2	+2152.8	+0010.0												
0000750	3	+0097.5	+0606.5	+0606.5	+0560.2	+0556.8	+0667.0	+0221.6	+0078.1	+0010.0	+0003.5	+2152.7	+0010.0												
0000750	3	+0097.4	+0606.3	+0606.4	+0560.1	+0556.8	+0667.0	+0221.8	+0078.1	+0010.0	+0003.2	+2152.8	+0010.0												
0000750	3	+0096.7	+0606.3	+0606.4	+0560.1	+0556.8	+0667.2	+0221.8	+0078.1	+0010.0	+0003.3	+2153.1	+0010.0												
0000751	3	+0096.8	+0606.2	+0606.4	+0560.1	+0556.9	+0667.2	+0221.5	+0078.2	+0010.0	+0003.4	+2151.8	+0010.0												
0000751	3	+0096.8	+0606.2	+0606.4	+0560.2	+0557.0	+0667.1	+0221.2	+0078.2	+0010.0	+0003.2	+2151.0	+0010.0												
0000751	3	+0097.0	+0606.3	+0606.3	+0560.1	+0557.0	+0667.1	+0221.0	+0078.2	+0010.0	+0003.7	+2150.7	+0010.0												
0000751	3	+0096.9	+0606.2	+0606.2	+0559.9	+0556.9	+0667.1	+0220.7	+0078.3	+0010.0	+0003.4	+2148.7	+0010.0												
0000751	3	+0096.9	+0606.1	+0606.2	+0560.0	+0556.9	+0667.2	+0220.3	+0078.3	+0010.0	+0003.4	+2148.5	+0010.0												
0000751	3	+0096.8	+0606.0	+0606.2	+0560.1	+0556.8	+0667.4	+0220.0	+0078.3	+0010.0	+0003.5	+2147.6	+0010.0												
0000751	3	+0096.8	+0606.0	+0606.1	+0559.7	+0556.7	+0667.3	+0219.7	+0078.3	+0010.0	+0003.0	+2147.0	+0010.0												
0000751	3	+0096.9	+0606.0	+0606.1	+0559.7	+0556.7	+0667.0	+0219.3	+0078.3	+0010.0	+0003.7	+2147.2	+0010.0												
0000751	3	+0096.8	+0606.0	+0606.1	+0559.8	+0556.7	+0667.0	+0219.1	+0078.3	+0010.0	+0003.2	+2146.8	+0010.0												
0000751	3	+0096.8	+0605.9	+0606.0	+0559.8	+0556.7	+0667.1	+0218.7	+0078.3	+0010.0	+0003.5	+2145.0	+0010.0												
0000751	3	+0096.8	+0605.9	+0605.9	+0559.7	+0556.7	+0667.5	+0218.1	+0078.3	+0010.0	+0003.3	+2143.9	+0010.0												
0000751	3	+0096.8	+0605.9	+0605.9	+0559.7	+0556.4	+0667.5	+0218.3	+0078.2	+0010.0	+0003.2	+2144.8	+0010.0												
0000751	3	+0096.7	+0605.8	+0605.9	+0559.6	+0556.5	+0667.6	+0217.8	+0078.2	+0010.0	+0003.6	+2142.9	+0010.0												
0000751	3	+0096.7	+0605.8	+0605.8	+0559.5	+0556.4	+0667.0	+0217.6	+0078.1	+0010.0	+0003.0	+2142.5	+0010.0												
0000751	3	+0096.7	+0605.8	+0605.8	+0559.5	+0556.4	+0667.0	+0217.3	+0078.1	+0010.0	+0003.5	+2142.8	+0010.0												
0000751	3	+0096.7	+0605.7	+0605.7	+0559.4	+0556.5	+0667.0	+0217.2	+0078.0	+0010.0	+0003.0	+2142.8	+0010.0												
0000751	3	+0097.4	+0605.7	+0605.7	+0559.4	+0556.4	+0666.9	+0216.9	+0077.9	+0010.0	+0003.2	+2142.0	+0010.0												
0000751	3	+0097.3	+0605.4	+0605.7	+0559.3	+0556.4	+0667.0	+0216.9	+0077.9	+0010.0	+0003.5	+2142.2	+0010.0												
0000751	3	+0097.2	+0605.7	+0605.8	+0559.1	+0556.1	+0667.0	+0216.9	+0077.9	+0010.0	+0003.0	+2142.9	+0010.0												
0000751	3	+0097.3	+0605.6	+0605.8	+0559.3	+0556.1	+0667.2	+0216.9	+0077.8	+0010.0	+0003.4	+2143.8	+0010.0												
0000752	3	+0097.3	+0605.6	+0605.8	+0559.1	+0556.1	+0667.2	+0217.3	+0077.7	+0010.0	+0003.3	+2143.7	+0010.0												
0000752	3	+0097.3	+0605.6	+0605.8	+0559.3	+0556.0	+0667.3	+0217.2	+0077.6	+0010.0	+0003.0	+2142.5	+0010.0												
0000752	3	+0097.2	+0605.6	+0605.8	+0559.2	+0556.1	+0667.2	+0217.3	+0077.6	+0010.0	+0003.5	+2143.8	+0010.0												
0000752	3	+0097.2	+0605.6	+0605.8	+0559.4	+0556.1	+0667.5	+0217.7	+0077.5	+0010.0	+0003.0	+2144.5	+0010.0												
0000752	3	+0097.3	+0605.7	+0605.8	+0559.2	+0556.0	+0667.3	+0217.9	+0077.4	+0010.0	+0003.3	+2143.9	+0010.0												
0000752	3	+0097.3	+0605.7	+0605.9	+0559.5	+0556.1	+0667.1	+0218.0	+0077.4	+0010.0	+0003.0	+2146.0	+0010.0												
0000752	3	+0097.3	+0605.7	+0605.9	+0559.5	+0556.2	+0667.2	+0218.3	+0077.3	+0010.0	+0003.4	+2146.4	+0010.0												
0000752	3	+0097.3	+0605.7	+0605.9	+0559.5	+0556.2	+0667.2	+0218.3	+0077.3	+0010.0	+0002.9	+2143.9	+0010.0												
0000752	3	+0097.2	+0605.8	+0605.9	+0559.3	+0556.3	+0667.0	+0218.5	+0077.3	+0010.0	+0003.4	+2146.9	+0010.0												
0000752	3	+0097.2	+0605.8	+0606.0	+0559.3	+0556.4	+0666.9	+0218.7	+0077.2	+0010.0	+0003.2	+2147.6	+0010.0												
0000752	3	+0097.3	+0605.8	+0606.0	+0559.3	+0556.5	+0667.1	+0218.9	+0077.2	+0010.0	+0003.2	+2148.1	+0010.0												
0000752	3	+0097.3	+0605.8	+0606.0	+0559.1	+0556.4	+0667.2	+0219.2	+0077.2	+0010.0	+0003.4	+2147.5	+0010.0												

K-8

History of R1 Power Aug 30 - Nov 30 1978



K-9 RCB Pressure from
 Strip Chart Used as pressure
 correction to Peak Rate calculations & done in
 2142 ¹⁹⁸⁰

78

1	2/20	8:05	(flue 2125-2155)	7:05	(flue 2115-2155)
21		2:59	2142	3:59	2142
22		8:10	2130-2150	8:10	2160-2180
22		23:26	2120-2155	23:00:26	2120-2165
23		20:48	2130-2160	21:48	2130-2160
24		17:30	(flue 2125-2185)	18:30	(2115-2185)
25		1:20	2130-2140	2:20	2150-2185
25		7:52	2130-2185	8:52	2130-2180
26		2:49	2120-2190	3:49	2120-2190
26		9:16	2145-2200	10:16	2140-2190
27		8:10	Mudding	9:10	Mudding
30		6:15	2120-2150	7:15	2120-2160
31		5:17	2120-2145	6:17	2120-2145
31		12:25	2120-2150	13:25	2120-2150
79	1/2	1:03	2120-2155	2:03	2125-2155
4		3:02	2140	4:02	2145-2165
5		2:54	2130-2150	3:54	2130-2160
5		17:23	2120-2180	18:23	2120-2180
6		2:47	2120-80	3:47	2120-80
6		10:29	2120-80	11:29	2130-2155
6		19:20	2125-80	20:20	2110-2200
7		3:46	2120-2180	4:41	2130-2170
8		3:21	2120-2155	4:21	2130-2160
8		6:21	2125-2155	7:21	2120-2165
10		1:48	2120-2155	2:48	2120-2165
11		21:53	2130-2155	22:53	2130-2155
13		9:37	2130-2155	10:37	2130-2155
15		0:24	2145	1:24	2145

all 2100+ P91

④ 1/30	22:06	missing	23:06	missing
2/2	0:55	20-40	1:55	20-40
2	14:31	20-40	15:31	20-40
3	5:17	20-40	6:17	20-40
3	10:32	10-50	11:32	20-35
3	23:49	20- 60	0:49	40-50
4	14:45	20-30	15:45	20-45
5	3:12	20-70	4:12	20-55
5	8:35	20-40	9:35	15-40
5	18:37	20-40	19:37	05-80
6	0:25	2100-2180	1:25	2100-2180
7	1:50	10-30	2:50	10-30
7	13:38	20-30	14:38	20-30
8	20:50	30-40	21:50	25-35
8		2115	21:50	2115-2130
9	2:20	20-40	3:20	20-40
10	8:41	20-40	9:41	15-30
11	2:41	25-40	3:41	25-40
11	18:08	2135	19:08	2135
12	21:20	15-25	22:20	2125
13	12:36	2100-2135	13:36	2115-2135
13	18:42	2120-2140	19:42	2127
14	5:30	2128	0:30	2128
14	20:46	20-40	21:46	20-30
15	20:20	2125	21:26	15-40
16	1:53	15-40	2:53	50-70
16	12:03	2100-2110	13:03	2130
17	4:11	2120	5:11	2120

2/19 0:01 2/25 1:01 15-30

(79) ~~2/19~~ ~~0:01~~ ~~2/25-2/25~~ ~~1:01~~ ~~15-30~~

~~19 1:36~~ ~~21 8:36~~ ~~2/25-2/25~~ ~~21:36~~ ~~15-30~~
~~20 2:28~~ ~~21 2:20~~ ~~21:20~~ ~~21:20~~ ~~21:20~~
~~21 8:36~~ ~~20-50~~ ~~21:36~~ ~~20-35~~

~~23 11:07~~ ~~21:20~~ ~~12:07~~ ~~21:20~~

~~25 20:02~~ ~~10-25~~ ~~21:02~~ ~~21:00-21:30~~

~~26 0:38~~ ~~21:28~~ ~~1:38~~ ~~25-35~~

~~26 18:39~~ ~~2080-2130~~ ~~19:39~~ ~~21:22~~

~~27 21:50~~ ~~10-20~~ ~~22:50~~ ~~10-20~~

~~28 19:24~~ ~~21:25~~ ~~20:24~~ ~~10-20~~

~~2/1 0:41~~ ~~1:41~~ ~~2:41~~ ~~10-20~~
~~4 1:41~~ ~~2:42~~
~~6 3:21~~ ~~4:21~~
~~8 3:06~~ ~~4:06~~
~~12 1:32~~ ~~2:32~~
~~13 2:00~~ ~~3:00~~
~~14 12:05~~ ~~13:05~~
~~15 4:50~~ ~~5:50~~
~~16 20:09~~ ~~21:09~~
~~17 2:48~~ ~~3:48~~
~~21 1:14~~ ~~2:14~~
~~25 5:25~~ ~~6:25~~
~~28 1:34~~ ~~2:34~~
~~28 19:09~~ ~~20:09~~

10
23
25
27
88

3/1/79

	0:41	2125		1:41	35-60
2	1:46	Missing		2:46	Missing
2	19:35	2140		20:35	2140
3	2:38	2140		3:38	2140
4	1:42	2140		2:42	2140
5	3:20	2140		4:20	2140
6	3:21	20-50		4:21	40-50
8	3:06	2140		4:06	2140
9	3:23	2140		4:23	2140
10	3:51	40-50		4:51	2140
12	1:32	2145	2:32		2145
13	2:0	2140	3:0		2140
13	11:05	30-50	12:05		30-50
14	12:05	2145	13:05		2145
15	4:50	2145	5:50		2145
16	20:09	2130	21:09		2130
17	2:48	2150	3:48		2150
19	0:58	40-50	1:58		40-50
21	1:14	2140	2:14		35-45
22	3:00	2150	4:00		2150
24	5:40	2140	6:40		2140
25	5:25	2135	6:25		2135
28	1:34		2:34		

150 gal

20

62.3

40° var

20±

3

05

.05

5%

10⁸ 10⁹ 10¹⁰
1% 1%

Trailer 202 John ~~W~~ Saunders
60-61 8482
Marell 8299

Bin 28 Pt # 23 MUT

K-10

REACTOR COOLANT SYSTEM LEAK RATE TESTING IN PWRs.

A number of concerns regarding the adequacy of the primary system leak rate determinations in PWRs were identified during a recent investigation. These include inaccuracy in the test results, errors in the computer program used for the leak rate calculations and personnel actions affecting the test results.

A. Variation in the Test Results

A plot of the leak rate test results had a scatter that exceeded the allowable unidentified leak rate of one gpm. Several causes of potentially large variation were identified, including:

1. The normal inaccuracy in the instrumentation.
2. Variation in the temperature distribution in the primary system.
3. Variation in the input parameters during the time that the data is being taken.

The test procedure is always conducted over a period of one hour, with the result that a discrepancy of 60 gallons in the water inventory can cause an apparent limiting leak rate. The makeup tank level normally oscillates over a level change of about $1\frac{1}{2}$ inches with a frequency on the order of one to two minutes. The beginning and end input data sets consist of three measurements, taken at one minute intervals and averaged. This

results in a variation of over an inch in the makeup tank level measurement. Since an inch change in this tank is equivalent to over 40 gallons at reactor temperature, this error alone approaches the one gpm leak rate limit. A 0.5°F error in the difference between the beginning and end averaged RCS temperature will also result in a leak rate error of about 1 gpm. This value appears to be comparable to the expected error which is subject to all three of the effects listed above at both the beginning and end of the one hour measurement.

B. Errors in the Computer Program

A number of significant errors were identified in the computer program used to perform the leak rate calculations as follows:

1. The densities used to determine gallons of gross leakage and gallons of identified leakage are not consistent. The gross leakage from the RCS is determined by summing the RCS mass changes in pounds (makeup tank included) and multiplying by a gallons-per-pound factor which is based on the average RCS temperature (.16787 gallons/# at 582°F, see item 5 below.) The identified leakage, however, is derived directly from the leakage collection tank level change, converted to gallons. The calibration for this level measurement is based on a cold water density of 62.3099 #/ft³ (.1200⁷ gallons/# at ^{70°F} ambient temperature). The unidentified leakage is defined as gross leakage less identified leakage. This inconsistency led to a positive error in the unidentified leak rate of about 40% of the identified leak ra

2. Water added by the operators to the makeup tank during the test (which must be manually entered into the computer), also was not corrected to reactor density, resulting in a negative error of similar magnitude.

3. The conversion of RCS average temperature to density is erroneous above 582°F. The tables in the program used to convert temperature to density terminate at 582°F. When RCS temperature exceeds this value, the density corresponding to 582°F is selected. The test data reviewed, frequently contained temperatures above 582°F resulting in errors as high as one gpm.

4. No correction was made for pressure changes in the RCS during the test. Pressure affects the coolant mass determination in several ways, the largest being the change in pressurizer mass due to the resulting change in pressurizer temperature. During some of the test periods reviewed, the RCS pressure was cycling over a range of 80 psi resulting in density changes of 0.63 pounds per cubic foot. With an 800 cubic foot pressurizer water volume, this omission resulted in an error of about 1.3 gpm.

5. The computer program uses a density derived from the average RCS temperature, for conversion of RCS mass change to gallons of leakage. However, the SAR derivation of the allowable unidentified leakage uses a cold leg density of 46.4 #/ft³.

6. The RCS volume used in the program does not correspond to the SAR values.

7. The table in the program used to convert the reactor coolant leakage collection tank levels to gallons of water does not correspond to similar tables in the leakage surveillance procedure used for hand calculations.

C. Personnel Actions Affecting the Leak Rate Test Results.

Several personnel actions which changed the outcome of the leak rate test results were also identified:

1. As a result of the problems identified above, the scatter in the leak rate test results exceeded the allowable unidentified leak rate. Consequently, many of the leak rate tests showed unidentified leakage in excess of the allowable leak rate, regardless of the actual leakage. A common personnel practice was to ignore such high leak rates and to continue running leak rate tests until a result below the limit was achieved. Personnel considered the acceptance criteria to have been met if any of these tests met the limit prior to the end of the 72 hour surveillance period. The plant technical specifications require reduction of the leakage to within allowable limits within four hours or shutdown to hot shutdown within the next six hours.

2. On various occasions personnel added water to the makeup tank during the test, without entering the addition into the computer calculation of the leak rates. These additions were identified by log entries and confirmed by examination of the makeup tank level recorder charts.

3. Personnel increased the makeup tank hydrogen cover gas pressure during tests causing an increase in the indicated makeup tank level. While the level indication is nominally unaffected by changes in the cover gas pressure, the stated increase was confirmed by examination of the makeup tank level recorder chart. The cause of the indicated level change is believed to be a manometer effect from condensation in the normally dry reference leg.

*include
case* →

ACTIONS TO BE TAKEN BY LICENSEES OF ALL PWR FACILITIES WITH OPERATING LICENSES

A. Error analysis

Please provide an error analysis of the primary system leak rate calculation based on standard variation. Use the time period normally used to conduct the test. Include in the analysis, the estimated variation in each of the parameters that are used as input data to the calculation. The estimated variation should include:

1. Instrument variation between beginning and final data sets (repeatability). Compare these values to the ranges of the respective instruments.
2. The effect of hysteresis on level measurements.
3. The effect of real variation in the measured parameters during the time period over which a data set is being taken.
4. The effect of temperature distribution changes on the measured average temperatures in the RCS.

5. The effect^{of} any potentially significant changes to the primary system that are not accounted for in the leak rate calculations. In particular, include the effect of temperature variation in the pressurizer, the makeup tank, and^{the} primary leakage collection tank if these are not accounted for by the calculation.

Please provide, as part of the submittal, the details of the above analysis, including the estimated variations listed above.

B. Review of Computer Calculation

Please review the computer program used to calculate the RCS leak rate test results. Determine if any of the errors listed in the description of the computer problems above exist in your program. Include a description of this computer program as part of the submittal. Include as part of this description:

1. The basic equations used to calculate the various leak water rates
2. Various constants used in the calculation and their derivation. In particular, include all constants used to convert level and temperature changes in the RCS, pressurizer, makeup tank and RCS leakage collection tank, to volume and/or mass changes.
3. The equations or tables used to derive water density/ specific volume from temperatures and (if applicable) pressure.

- 1 -

4. The data collection scheme, including the number of times each parameter is collected, the times of collection relative to the start of the test, and the method of averaging data.

5. List any errors identified in the computer program.

C. Personnel Actions

Please provide information relative to your facilities in the following areas:

1. Any significant difficulties that you are experiencing in achieving test result accuracies that are commensurate with the allowable limits.
2. Any special treatment of the leak rate test results, such as, plotting, trending or error analysis used to assure that leakages are within limits.
3. Your policy on the course of action to be followed when a leak rate test indicates leakage in excess of the allowable limits.
4. Administrative controls to prevent the addition of water to the RCS without entry into the leak rate calculation.
5. The sensitivity of the makeup tank and primary leakage collection tank level measurement to pressure changes. Indicate if actions to change the pressure in these tanks is permitted during a leak rate test.

For all power reactor facilities with a construction permit, this Bulletin is for information only and no written response is required.

Approved by GAO B180225 (R0072); clearance expires 7-31-80. Approval is given under a blanket clearance specifically for identified generic problems.

K-11

DRAFT

RCSLK8
REACTOR COOLANT SYSTEM LEAK RATE DETERMINATION
FOR PWRs
USER'S GUIDE

D. C. Kirkpatrick & R. W. Woodruff

March 24, 1983

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INTRODUCTION

RCSLK8 was developed to provide the inspector with the capability to independently analyze the leak tightness of reactor cooling systems for PWRs. Using operating data, RCSLK8 determines the water inventories in the reactor cooling system and in leak collection tanks. By taking two sets of data separated by a time interval and applying RCSLK8, the inspector can obtain the gross leak rate for the reactor cooling system and the rate at which leakage is collected.

Collected or identified leakage comes from components such as valves and seals. Uncollected or unidentified leakage may come from components or from thru-wall flaws in reactor cooling piping. This leakage spills on containment building floors and, depending on the location of the leak and the rate, will reach the containment sump sooner or later. To determine the unidentified leak rate, RCSLK8 subtracts the identified leak rate from the gross leak rate.

Thru-wall flaws may gradually grow until the critical flaw size is exceeded. If that were to happen, it is conceivable that the flaw might suddenly extend resulting in rapid loss of coolant. To provide assurance that thru-wall flaws will be detected early, a limiting condition for operation (LCO) in PWR technical specifications addresses unidentified leakage from the reactor cooling system. If the source of leakage from the reactor cooling system is unknown, then it must be assumed that the source may be from a thru-wall flaw. The LCO for unidentified leak rate is one gpm for most PWRs. Identified leakage cannot be from thru-wall flaws, and the LCO for this leakage is more lenient.

RCSLK8 was developed for use with the Osborne 1 computer. The Osborne was selected because it has adequate internal memory and diskette storage for RCSLK8, is portable, and is likely to meet our needs for other independent measurement programs for some time to come.

To apply RCSLK8 to a specific unit for the first time, it is first necessary to obtain certain information about the plant and enter this information in the computer's memory. Once that is done, RCSLK8 commands the computer to store the information indefinitely on the RCSLK8 PROGRAM diskette. RCSLK8 can then be used to analyze the leak tightness of the unit's cooling system at any time. At the inspector's option, a report of the analysis will be displayed on the computer's monitor or will be printed with a compatible printer.

because of leaks and because water can be supplied to and withdrawn from these systems. Water can be supplied to the CVCS thru a totalizer or flow integrator. The total volume supplied in any period of time is determined by reading the totalizer at the beginning and end of the period and taking the difference. Water may also be withdrawn from the system for sampling purposes. This volume can be measured directly.

Leakage from certain RCS components is collected in either the pressurizer relief tank or the reactor drain tank. However, at some plants, water from sources other than the RCS and CVCS may be piped to the reactor drain tank. These lines must be valved off during a leak rate test.

Water levels in the pressurizer relief and reactor drain tanks are also determined by measuring delta-Ps between upper and lower taps. The level instruments for these tanks are not temperature compensated. Generally, these tanks are cylindrical with convex heads. Often, the tanks are oriented so that their axes are horizontal.

Level instrumentation may be calibrated by pneumatically applying a range of delta-Ps across the level instrument and reading its response. The applied delta-P is converted to head of water by dividing the delta-P by the density of water at the normal operating temperature of the tank. This temperature is called the calibration temperature. Either the volume or the mass of water corresponding to this head is calculated and the calibration curve is plotted. This curve is usually a plot of water mass or volume versus indicated level in inches or percent of full range. Uncompensated level instrumentation and a correct mass calibration curve give accurate results for the mass of water in the tank at any temperature. Uncompensated level instrumentation and a correct volume calibration curve give accurate results for the volume of water in the tank only when the water is at the calibration temperature. The reverse is true for compensated level instrumentation.

For a vertical tank, the calibration curve is linear for the cylindrical portion of the tank, and usually, the cylindrical portion of the tank is long relative to the height of the heads. For a horizontal tank, the calibration curve is, in principle, nonlinear. In reality, however, the central part of the curve is essentially linear. For some tanks, the normal operating range falls within the linear part of the calibration curve, and for others it does not. If not, the mass of water in the tank must be calculated from tank dimensions, water level, and water density.

be used to convert from mass leak rate to volume leak rate; however, since the point of leakage is not known, the density is not known. Further, limiting conditions for operation do not specify the value of density that should be used in converting mass leak rate to volume leak rate. RCSLKB asks the user to arbitrarily select the conditions which determine the density. RCSLKB then calculates the gross leak rate. The result of the gross leak rate calculation is shown under TEST RESULTS which includes a footnote giving the value of water density that was used in converting from mass to volume.

The input required for calculating the gross leak rate is given under TEST DATA and under DURATION. Test data that are needed are pressurizer pressure and level, T ave, volume control tank level, the volumes of water charged and drained.

In addition to these data, the values of certain plant specific parameters are needed before the gross leak rate can be calculated. These parameters are:

- (a) Water volume of the reactor vessel, pumps, steam generators, and connecting piping, including the piping to the pressurizer;
- (b) Slopes of the linear portion of the calibration curves for the pressurizer and the volume control tank; and
- (c) Upper and lower level limits for the linear portions of the calibration curves.

In addition, the inspector will need to know whether the level instrumentation for the pressurizer is temperature compensated, the tank to which the pressurizer relieves, the units of measurement for the level instrumentation, and whether the normal operating range for the volume control tank falls within the linear portion of its calibration curve. If the normal operating range does not and if the tank is cylindrical and horizontal, then the inside dimensions of the tank and the density of water at the calibration temperature will be needed. The water volume can then be calculated using the method described in Appendix D.

Identified Leak Rate

To determine the identified leak rate for the RCS and CVCS during the test, the amount of water collected in the pressurizer relief tank and the reactor drain tank must be calculated. Prior to the test, the inspector must make certain that no drains other than RCS and CVCS drains are connected to the reactor drain tank. If leakage is collected from other systems, then the identified leak rate will be too large and the unidentified leak rate will be too small.

If the inspector calculates the unidentified leak rate using the same test data that the licensee has used and if the results differ by more than 0.2 gpm, the inspector should try to determine the cause of the discrepancy. Assistance can be obtained from Inspection and Enforcement. After the cause for the discrepancy is determined, corrective action should be taken.

CREATION AND FUNCTION OF RCSLK8 SOFTWARE

RCSLK8 is stored on two 5 1/4 inch diskettes. One diskette, labeled RCSLK8 PROGRAM, stores all the subroutines necessary to run RCSLK8. The other diskette, labeled RCSLK8 USER'S GUIDE, stores this document.

RCSLK8 PROGRAM contains AUTOST.COM, other CP/M subroutines needed to run RCSLK8, CRUN2.COM, H.INT, RCSLK8.INT, and files of PWR parameters created by running RCSLK8. As supplied to the regions with this issue of the User's Guide, the parameter files written on the RCSLK8 PROGRAM diskette are: 255, 266, 282, 295, 301, 304, 305, 306, 312, 315, 316, 317, 318, 320, 344, 346, and 348. These file names are the last three digits of the docket numbers of certain PWRs. User's can create additional parameter files and correct existing parameter files by running the RCSLK8 PROGRAM diskette.

When the machine is turned on, the program stored in ROM takes control of the machine and displays a message or prompt on the monitor which asks the inspector to insert a program diskette in the A drive and press the RESET key. When the user responds to this prompt using the RCSLK8 PROGRAM diskette, CP/M subroutines stored on the diskette take control of the machine and invoke AUTOST.COM. AUTOST.COM (autostart command) automatically displays the NRC label, identifies the diskette as an independent measurements program, and directs the machine to use CRUN2.COM to run H.INT. H.INT in turn directs the machine to run RCSLK8.INT.

RCSLK8.BAS was written in CBASIC and is reproduced in Appendix A. RCSLK8.INT was compiled from RCSLK8.BAS by using CBAS2.COM from the CBASIC diskette. Compiling RCSLK8.BAS translated it from CBASIC language to intermediate language. RCSLK8.INT requires approximately half the storage space required by RCSLK8.BAS, and it runs faster. Likewise, H.INT was compiled from H.BAS which is reproduced in Appendix C.

The C/M subroutines necessary to run RCSLK8 were transferred from the CP/M diskette by running SETUP.COM, a CP/M subroutine.

AUTOST.COM for RCSLK8 was created by first using PIP.COM from CP/M to copy AUTOST.COM from the CP/M diskette to the RCSLK8 PROGRAM diskette. Then DDT.COM from CP/M UTILITY was used to modify AUTOST.COM for use with Independent Measurements programs. The original version of AUTOST.COM is given on pages 247 thru 250 of "Osborne 1 User's Reference Guide" dated 2/22/82. The modified version is given in Appendix B.

- (a) Nominal operating level and
- (b) Pressurizer volumes above and below the nominal operating level.

For each tank including the pressurizer, the computer will ask for:

- (a) Units for level measurement,
- (b) Slope of the linear portion of the calibration curve for volume or mass versus level, and
- (c) Upper and lower level limits of the linear portion of the calibration curve.

For all tanks except the temperature-compensated pressurizer, the computer will ask for the slope in pounds of water per unit level change. If the licensee's calibration curve is in volume of water per unit level change, the inspector will need to convert from volume to mass of water. That should be done by obtaining from the licensee the density of water assumed for the calibration and using that value to convert the slope from volume per unit level change to mass per unit level change.

If the user wishes to enter the dimensions of any horizontal tank, the computer will ask for:

- (a) Radius and length of the cylindrical part of the tank,
- (b) Radius of the heads of the tank, and
- (c) Density of water at the calibration temperature.

The computer will then calculate the mass of water between the upper and lower limits of the straight line portion of the calibration curve in two different ways. First, it will do the calculation using the calibration curve, and second, it will do the calculation using the tank dimensions and the water density at the calibration temperature (geometric method). The computer will take the ratio of the first result to the second, label the ratio as the normalization factor, display the normalization factor and store it for future use. Whenever, the user directs the computer to calculate a water inventory in a tank by using the geometric method, the computer will multiply the result by the normalization factor.

After keying each information item into the computer in response to its requests, the user must strike the RETURN key in order to continue. Once the RETURN key is struck, the entry cannot be corrected until after the plant parameter entry session is completed. When the user returns to the options menu, corrections can be made with ease by invoking the correction subroutine. Before doing this, the user may want to list the plant parameters as entered. All values of parameters that are now stored on the RCLSK8 PROGRAM diskette are shown in Appendix F.

stores the normalization factor. The computer then asks if there are other corrections for that group. If so, the parameter menu is displayed again. If not, the user is asked if there are corrections for other groups. If so, the group menu is displayed again. If not, the computer, asks whether to continue or terminate the session.

Listing Plant Parameters

By selecting from the options menu the option for listing the values of plant parameters, the user can obtain a list for any unit for which a file has been created. The list can either be printed or displayed on the monitor. If it is displayed on the monitor, the computer will list the parameters on the screen until it is filled and then stop until the user directs the computer to resume listing. When the list is completed, the computer will ask whether to continue or terminate the session.

Identifying Plants with Parameters on File

When the options menu is displayed, the user can direct the computer to search its files for all units for which parameter files have been created. The computer will respond by searching for docket numbers from 50-029 to 50-599. Because this takes a few minutes, each docket number is displayed as the computer searches for it. In this way the user knows that computer is functioning. If a printer is used, each time a file is found the docket number, plant name, and unit number will be printed. If a printer is not used, this information will be displayed on the screen. If plant name and unit number are not displayed, then a file for that unit does not exist. A list of files now available on the RCSLKB PROGRAM diskette is given in Appendix E.

Calculating Leak Rates

After a parameter file has been created for a specific unit, the leak tightness of the RCS and CVCS can be analyzed by calculating the gross, identified, and unidentified leak rates. When the data analysis subroutine of RCSLKB is initiated, the computer first asks for the test date and the start time for the test. This information is obtained for archival purposes for a printed report. The user should note that test data are not saved on the diskette.

The computer then asks for the duration of the test in hours. Because the accuracy of the test is directly proportional to the test duration, the minimum duration should be four hours.

After the duration is entered, the computer asks for the volumes

14,000 psia.

The water inventory in temperature-compensated pressurizers is found by calculating the mass of water and the mass of steam in the pressurizer. The mass of water is found by assuming that it is saturated. The computer finds the saturation temperature of the water by running the subroutine, Saturation Temperature, shown on pages A-25 and 26 of Appendix A. This is an iterative subroutine which duplicates the values given in Table 2 of the steam tables for pressures from 14.7 psia to 3208.2 psia. The density of saturated water is found by substituting pressurizer pressure and the saturation temperature in the subcooled water subroutine. The density of saturated steam is found from subroutine, Density of Saturated Steam, on page A-27 of the appendix. This is a curve fit to the steam tables with an accuracy of 1.0% or better in the range from 1400 to 2700 psia.

The inventories for other tanks are calculated from either the calibration curves or from the tank dimensions and the appropriate density. The rest of the analysis is performed as described in the section titled Water Inventories and System Leak Rates.

After the analysis is completed, a report of the results is displayed on the monitor or is printed with the printer.

PROCEDURE

Running RCSLK8

1. To prepare to run RCSLK8, place the Osborne 1 in the upright position, and open the cover adjacent to the handle. Remove the cord and connect the computer to an electrical outlet.
2. Place the case on its side with the ribbed side down and open the ventilation cover on the top side.
3. Unlatch the bottom of the case to release the keyboard. Place the lower edge of the computer on the upper edge of the keyboard.
4. If the Itoh printer will be used, connect the printer cable to the IEEE 488 port on the front of the computer. Connect the other end of the cable to the connector on the back of the printer.
5. Connect the printer to an electrical outlet.
6. Open the doors on both disk drives to make certain that neither drive contains a diskette.
7. Turn on power to the computer and to the printer.
8. Position the selector lever on the top of the printer to FRICTION.
9. Press the SEL (select) button on the front of the printer if the SEL light is not illuminated.
10. Place a piece of typing paper in the printer.
11. Move the selector lever to PIN-FEED. Align the left edge of the paper so that it is 3/8 inch to the left of the index on the roller shaft. Move the selector lever to FRICTION. Align the top edge of the paper with the rollers.
12. To run RCSLK8, follow the instructions displayed on the monitor. Latch the drive door before pressing the RETURN key.
13. Replace paper in the printer as necessary. If the computer does not function, make certain that there is paper in the printer and that the SEL light is on.
14. After the session is terminated and AFTER THE INDICATOR LIGHT OF THE "A" DRIVE IS OFF, open the drive door and remove the disk. If the indicator light is not off, information stored

RCCLK8.BAS


```

10  \
    \
    \
                                     *****
                                     * PLANT LIST *
                                     *****

A%=10  :  B%=20

PRINT TAB(21);"Searching" : PRINT
IF PRINT.FLAGS="Y" THEN LPRINTER : PRINT : PRINT : PRINT \
    : PRINT TAB(27);"PLANTS WITH PARAMETERS FILED" : PRINT \
    : PRINT
FOR D% = 29 TO 599
  D$=STR$(D%) : I$="A:"+D$ : CONSOLE
  PRINT TAB(23);"50-"; : PRINT USING "###";D%
  IF END #1 THEN 12
  OPEN I$ RECL 30 AS 1
  READ #1,1; PLANT$ : READ #1,2; UNIT$ : READ #1,45; DOCKET$
  IF PRINT.FLAGS="Y" THEN LPRINTER : A%=27 : B%=37
  PRINT TAB(A%);"50-";DOCKET$;TAB(B%);PLANT$;" ";UNIT$ : CONSOLE
  CLOSE 1
12  NEXT D%
    GOTO 995      REM: Continuation or Termination

```

```

PRINT "piping to the pressurizer and the inlet side of"
INPUT "the letdown heat exchanger:";VP.VOL : RETURN

70 \
      ** PRESSURIZER **

      TANK$ = "Pressurizer"
      GOSUB 260 : PZR.UNITS$ = UNITS$ : PRINT #1, 5; PZR.UNITS$
      GOSUB 75 : PRINT #1, 6; COMPS

      IF COMPS="Yes" THEN GOSUB 80 : GOSUB 90 : GOSUB 91 \
        : GOTO 71 ELSE GOTO 72

71 PRINT #1, 7; PZR.LVL.NOM : PRINT #1, 8; PZR.BTM.VOL
   PRINT #1, 9; PZR.TOP.VOL

72 GOSUB 270 : PZR.SLOPE=SLOPE : PRINT #1,10; PZR.SLOPE
   GOSUB 280 : PZR.UP.LMT=UP.LMT : PRINT #1,11; PZR.UP.LMT
   GOSUB 290 : PZR.LO.LMT=LO.LMT : PRINT #1,12; PZR.LO.LMT
   GOSUB 100 : GOTO 110

\
      * Temperature Compensation *

75 PRINT "Pressurizer level instrumentation may be:" : PRINT
   PRINT " (A) Temperature Compensated or"
   PRINT " (B) Uncompensated." : PRINT
   INPUT "Which is it (A/B)?";Y$

   PRINT : PRINT : PRINT

   IF Y$="A" THEN COMPS="Yes" : GOTO 77 ELSE GOTO 76
76 IF Y$="B" THEN COMPS="No" ELSE GOTO 75
77 RETURN

\
      * Nominal Level *

80 PRINT "For the Pressurizer, type the nominal operating"
   IF PZR.UNITS$="Inches" THEN GOTO 82 ELSE GOTO 81
81 IF PZR.UNITS$="%" THEN GOTO 83 ELSE GOTO 85
82 INPUT "level in inches:";PZR.LVL.NOM : GOTO 84
83 INPUT "level in %:";PZR.LVL.NOM

84 PRINT : PRINT : PRINT : RETURN

85 PRINT : PRINT "ERROR: Pressurizer units have not been entered."
   PRINT : PRINT : PRINT : GOTO 60

```

```

117 IF X$="B" THEN LD.TANK$="Makeup Tank" ELSE GOTO 116
118 RETURN

```

```

\
                ** DRAIN TANK **

```

```

120 TANK$ = "Drain Tank"
    GOSUB 260 : DT.UNITS$ = UNITS$ : PRINT #1,24; DT.UNITS$
    GOSUB 270 : DT.SLOPE=SLOPE : PRINT #1,25; DT.SLOPE
    GOSUB 280 : DT.UP.LMT=UP.LMT : PRINT #1,26; DT.UP.LMT
    GOSUB 290 : DT.LO.LMT=LO.LMT : PRINT #1,27; DT.LO.LMT
    GOSUB 300 : DT.GEO$=GEO$ : PRINT #1,28; DT.GEO$

    IF DT.GEO$="Yes" THEN GOSUB 310 : GOSUB 311 : GOSUB 312 \
                        : GOSUB 313 : GOTO 124 \
    ELSE GOTO 130

124 DT.CYL.RAD=CYL.RAD : PRINT #1,29; DT.CYL.RAD
    DT.CYL.LEN=CYL.LEN : PRINT #1,30; DT.CYL.LEN
    DT.CVX.RAD=CVX.RAD : PRINT #1,31; DT.CVX.RAD
    DT.DENSITY=DENSITY : PRINT #1,32; DT.DENSITY
    DT.NORMFAC=NORMFAC : PRINT #1,33; DT.NORMFAC

```

```

\
                ** RELIEF OR QUENCH TANK **

```

```

130 TANK$ =RQ.TANK$ : PRINT #1,34; RQ.TANK$

    IF RQ.TANK$="Drain Tank" THEN GOTO 135

    GOSUB 260 : RQT.UNITS$ = UNITS$ : PRINT #1,35; RQT.UNITS$
    GOSUB 270 : RQT.SLOPE=SLOPE : PRINT #1,36; RQT.SLOPE
    GOSUB 280 : RQT.UP.LMT=UP.LMT : PRINT #1,37; RQT.UP.LMT
    GOSUB 290 : RQT.LO.LMT=LO.LMT : PRINT #1,38; RQT.LO.LMT
    GOSUB 300 : RQT.GEO$=GEO$ : PRINT #1,39; RQT.GEO$

    IF RQT.GEO$="Yes" THEN GOSUB 310 : GOSUB 311 : GOSUB 312 \
                        : GOSUB 313 : GOTO 134 \
    ELSE GOTO 135

134 RQT.CYL.RAD=CYL.RAD : PRINT #1,40; RQT.CYL.RAD
    RQT.CYL.LEN=CYL.LEN : PRINT #1,41; RQT.CYL.LEN
    RQT.CVX.RAD=CVX.RAD : PRINT #1,42; RQT.CVX.RAD
    RQT.DENSITY=DENSITY : PRINT #1,43; RQT.DENSITY
    RQT.NORMFAC=NORMFAC : PRINT #1,44; RQT.NORMFAC

135 PRINT #1,45; DOCKET$

    CLOSE 1 : GOTO 995 REM: Continuation or Termination

```

```

311 PRINT "For the ";TANK$;" , type the length (feet)"
    INPUT "of the cylindrical part of the tank:";CYL.LEN
    GOSUB 314 : PRINT : PRINT : PRINT : RETURN

```

```

312 PRINT "For the ";TANK$;" , type the radius (feet)"
    INPUT "of the convex head:";CVX.RAD
    GOSUB 314 : PRINT : PRINT : PRINT : RETURN

```

```

\          * Water Density for Calibration *

```

```

313 PRINT "For the ";TANK$;" , type the density (pounds per"
    PRINT "cubic foot) of water assumed for the tank cali-"
    INPUT "bration:";DENSITY
    GOSUB 314 : PRINT : PRINT : PRINT : RETURN

```

```

314 IF CYL.RAD=0 OR CYL.LEN=0 OR CVX.RAD=0 OR DENSITY=0 THEN \
    NORMFAC=0 : RETURN ELSE GOTO 315

```

```

\          * Normalization Factor *

```

```

315 IF UNITS$ = "inches" THEN UP.LMT.FRAC=UP.LMT/(12*2*CYL.RAD) \
    ELSE UP.LMT.FRAC=UP.LMT/100

```

```

    IF UNITS$ = "inches" THEN LO.LMT.FRAC=LO.LMT/(12*2*CYL.RAD) \
    ELSE LO.LMT.FRAC=LO.LMT/100

```

```

    LVL.FRAC.I = LO.LMT.FRAC : LVL.FRAC.F = UP.LMT.FRAC
    GOSUB 871

```

```

    INV.CHG.GEO = INV.CHG
    INV.CHG.CAL = SLOPE*(UP.LMT-LO.LMT)
    NORMFAC = INV.CHG.CAL/INV.CHG.GEO
    PRINT TAB(10);TANK$ : PRINT TAB(12);"Normalization Factor is"
    PRINT TAB(14); : PRINT USING "#.####";NORMFAC
    PRINT : PRINT : PRINT
    INPUT "          To continue, press RETURN."; LINE X$
    RETURN

```



```
GOSUB 900 REM: Conditional Stop
```

```
\ ** VOLUME CONTROL OR MAKEUP TANK **
```

```
PRINT TAB(A%);LD.TANK$;":" : UNITS$=LDT.UNITS$
SLOPE=LDT.SLOPE : UP.LMT=LDT.UP.LMT : LO.LMT=LDT.LO.LMT
GEO$=LDT.GEO$ : CYL.RAD=LDT.CYL.RAD : CYL.LEN=LDT.CYL.LEN
CVX.RAD=LDT.CVX.RAD : DENSITY=LDT.DENSITY
NORMFAC=LDT.NORMFAC : GOSUB 490
GOSUB 900 REM: Conditional Stop
```

```
\ ** DRAIN TANK **
```

```
PRINT TAB(A%);"Drain Tank:"; : UNITS$=DT.UNITS$
SLOPE=DT.SLOPE : UP.LMT=DT.UP.LMT : LO.LMT=DT.LO.LMT
GEO$=DT.GEO$ : CYL.RAD=DT.CYL.RAD : CYL.LEN=DT.CYL.LEN
CVX.RAD=DT.CVX.RAD : DENSITY=DT.DENSITY
NORMFAC=DT.NORMFAC : GOSUB 490
```

```
IF RQ.TANK$="Drain Tank" THEN GOTO 480
GOSUB 900 REM: Conditional Stop
```

```
\ ** RELIEF OR QUENCH TANK **
```

```
PRINT TAB(A%);RQ.TANK$;":" : UNITS$=RQT.UNITS$
SLOPE=RQT.SLOPE : UP.LMT=RQT.UP.LMT : LO.LMT=RQT.LO.LMT
GEO$=RQT.GEO$ : CYL.RAD=RQT.CYL.RAD : CYL.LEN=RQT.CYL.LEN
CVX.RAD=RQT.CVX.RAD : DENSITY=RQT.DENSITY
NORMFAC=RQT.NORMFAC : GOSUB 490
GOSUB 900 REM: Conditional Stop
```

```
480 CLOSE 2 : CONSOLE
GOTO 995 REM: Continuation or Termination
```

```
\ ** TANK SUBROUTINE **
```

```
490 PRINT TAB(B%);"Level Units";TAB(D%);UNITS$
PRINT TAB(S%);"Calibration Curve"
PRINT TAB(C%);"Slope";TAB(E%);SLOPE;"pounds per ";LEFT$(UNITS$,4)
PRINT TAB(C%);"Upper Level Limit";TAB(E%);UP.LMT;UNITS$
PRINT TAB(C%);"Lower level limit";TAB(E%);LO.LMT;UNITS$
IF GEO$="Yes" THEN GOTO 491 ELSE GOTO 492
491 PRINT TAB(C%);"Water Density";TAB(E%);DENSITY;
PRINT "pounds per cubic foot"
492 PRINT TAB(B%);"Geometric Method Available";TAB(D%);GEO$
IF GEO$<>"Yes" THEN PRINT : RETURN ELSE GOTO 493
493 PRINT TAB(B%);"Dimensions"
PRINT TAB(C%);"Cylinder Radius";TAB(E%);CYL.RAD;"feet"
```



```

      : PRINT #2,8;0 : PRINT #2,9;0 : GOTO 597
IF X$="B" AND Y$="B" AND COMP$="Yes" THEN GOTO 597
IF X$="C" THEN GOSUB 80 : PRINT #2, 7; PZR.LVL.NOM : GOTO 597
IF X$="D" THEN GOSUB 90 : PRINT #2, 8; PZR.BTM.VOL : GOTO 597
IF X$="E" THEN GOSUB 91 : PRINT #2, 9; PZR.TOP.VOL : GOTO 597
IF X$="F" THEN GOSUB 270 : PZR.SLOPE=SLOPE \
      : PRINT #2,10 ; PZR.SLOPE : GOTO 597
IF X$="G" THEN GOSUB 280 : PZR.UP.LMT=UP.LMT \
      : PRINT #2,11 ; PZR.UP.LMT : GOTO 597
IF X$="H" THEN GOSUB 290 : PZR.LO.LMT=LO.LMT \
      : PRINT #2,12 ; PZR.LO.LMT : GOTO 597
IF X$="I" THEN GOSUB 100 : PRINT #2,34; RQ.TANK$ ELSE GOTO 530
IF RQ.TANK$="Drain Tank" THEN GOTO 537
IF RQ.TANK$="Relief Tank" OR RQ.TANK$="Quench Tank" THEN \
      TANK$=RQ.TANK$ : GOSUB 260 : PRINT #2,35; UNITS$ \
      : GOSUB 270 : PRINT #2,36; SLOPE : GOSUB 280 \
      : PRINT #2,37; UP.LMT : GOSUB 290 : PRINT #2,38; LO.LMT \
      : GOTO 597 ELSE GOTO 532

532 PRINT : PRINT "CODE ERROR: Tank for relieving Pressurizer not"
      PRINT "properly specified." : STOP

540 \      * Volume Control or Makeup Tank *

      ID% = 4 : READ #2,13; TANK$ : READ #2,14; UNITS$

      PRINT "The Volume Control or Makeup Tank parameters are:"
      PRINT : PRINT " (A) Tank Name," : PRINT " (B) Level Units,"
      PRINT " (C) Slope of the Calibration Curve,"
      PRINT " (D) Its Upper Level Limit,"
      PRINT " (E) Its Lower Level Limit,"
      PRINT " (F) Geometric Method," : PRINT " (G) Cylinder Radius,"
      PRINT " (H) Cylinder Length," : PRINT " (I) Head Radius, and"
      PRINT " (J) Water Density." : PRINT

      PRINT TAB(3);"NOTE: First correct (A) then (B) and"
      PRINT TAB(10);"then any other parameter(s) for"
      PRINT TAB(10);"this tank." : PRINT

      PRINT "Which do you wish to access (A/B/C/D/E/F/G/H/"
      INPUT "I/J)?" ;X$

      PRINT : PRINT : PRINT

      IF X$="A" THEN GOSUB 116 : PRINT #2,13; TANK$ : GOTO 597

      TANK$=LD.TANK$

      READ #2,15; SLOPE : READ #2,16; UP.LMT : READ #2,17; LO.LMT
      READ #2,18; GEO$ : READ #2,19; CYL.RAD : READ #2,20; CYL.LEN
      READ #2,21; CVX.RAD : READ #2,22; DENSITY

```

```

IF X$="I" THEN GOSUB 313 : PRINT #2,32; DENSITY : GOSUB 552 \
: GOTO 597 ELSE GOTO 550
552 PRINT #2,33; NORMFAC : PRINT : PRINT : PRINT : RETURN

560 \
      * Relief or Quench Tank *

ID% = 6 : READ #2,34; TANK$ : READ #2,35; UNIT$

PRINT "The Relief or Quench Tank parameters are:"
PRINT " (A) Tank Name," : PRINT " (B) Level Units,"
PRINT " (C) Slope of the Calibration Curve,"
PRINT " (D) Its Upper Level Limit,"
PRINT " (E) Its Lower Level Limit,"
PRINT " (F) Geometric Method," : PRINT " (G) Cylinder Radius,"
PRINT " (H) Cylinder Length," : PRINT " (I) Head Radius, and"
PRINT " (J) Water Density." : PRINT

PRINT TAB(3);"NOTE: First correct (A) then (B) and"
PRINT TAB(10);"then any other parameter(s) for"
PRINT TAB(10);"this tank." : PRINT

PRINT "Which do you wish to access (A/B/C/D/E/F/G/H/"
INPUT "I/J)?" ; X$

PRINT : PRINT : PRINT

IF X$="A" THEN GOSUB 100 : PRINT #2,34; TANK$ : GOTO 597

IF TANK$="Drain Tank" THEN GOTO 597

READ #2,36; SLOPE : READ #2,37; UP.LMT : READ #2,38; LO.LMT
READ #2,39; GEO$ : READ #2,40; CYL.RAD : READ #2,41; CYL.LEN
READ #2,42; CVX.RAD : READ #2,43; DENSITY

IF X$="B" THEN GOSUB 260 : PRINT #2,35; UNIT$ : GOTO 597
IF X$="C" THEN GOSUB 270 : PRINT #2,36; SLOPE : GOTO 597
IF X$="D" THEN GOSUB 280 : PRINT #2,37; UP.LMT : GOTO 597
IF X$="E" THEN GOSUB 290 : PRINT #2,38; LO.LMT : GOTO 597
IF X$="F" THEN GOSUB 591 : GOTO 597
IF X$="G" THEN GOSUB 310 : PRINT #2,40; CYL.RAD : GOSUB 562 \
: GOTO 597
IF X$="H" THEN GOSUB 311 : PRINT #2,41; CYL.LEN : GOSUB 562 \
: GOTO 597
IF X$="I" THEN GOSUB 312 : PRINT #2,42; CVX.RAD : GOSUB 562 \
: GOTO 597
IF X$="J" THEN GOSUB 313 : PRINT #2,43; DENSITY : GOSUB 562 \
: GOTO 597 ELSE GOTO 560

562 PRINT #2,44; NORMFAC : PRINT : PRINT : PRINT : RETURN

```



```

600 \ *****
\ * DATA ANALYSIS *
\ *****
\
\ ** DATA INPUT **

OPEN "A:"+DOCKET$ RECL 30 AS 2
IF END #2 THEN 3
GOSUB 890

INPUT "Type test date in quotes:";DATE$
INPUT "Type test start time in quotes:";TIME$
INPUT "Type test duration in hours:";DURATION
PRINT : PRINT : PRINT
PRINT "Type the quantity of water in gallons--" : PRINT
INPUT "                               Charged: ";GAL.CHARGED
INPUT "                               and Drained: ";GAL.DRAINED
PRINT : PRINT : PRINT

LDT.METHOD$="Cal" : DT.METHOD$="Cal" : RQT.METHOD$="Cal"
LDT.NOTE$="(1)" : DT.NOTE$="(1)" : RQT.NOTE$="(1)"
IF LDT.GEO$="Yes" OR DT.GEO$="Yes" OR RQT.GEO$="Yes" THEN \
GOTO 605 ELSE GOTO 610

605 PRINT "For the following tank(s), select either the"
PRINT "Calibration (C) or the Geometric (G) Method for"
PRINT "calculating water inventories." : PRINT
IF LDT.GEO$="Yes" THEN PRINT " ";LD.TANK$;" " ; ELSE GOTO 606
INPUT "(C/G)?";X$
IF X$="C" THEN LDT.METHOD$="Cal" ELSE LDT.NOTE$="(2)"
IF X$="G" THEN LDT.METHOD$="Geo"
IF X$<>"C" AND X$<>"G" THEN GOTO 605
606 IF DT.GEO$="Yes" THEN PRINT " Drain Tank "; ELSE GOTO 607
INPUT "(C/G)?";X$
IF X$="C" THEN DT.METHOD$="Cal" ELSE DT.NOTE$="(2)"
IF X$="G" THEN DT.METHOD$="Geo"
IF X$<>"C" AND X$<>"G" THEN GOTO 606
607 IF RQT.GEO$="Yes" THEN PRINT " ";RQ.TANK$;" " ; ELSE GOTO 610
INPUT "(C/G)?";X$
IF X$="C" THEN RQT.METHOD$="Cal" ELSE RQT.NOTE$="(2)"
IF X$="G" THEN RQT.METHOD$="Geo"
IF X$<>"C" AND X$<>"G" THEN GOTO 607

610 PRINT : PRINT : PRINT : A% = 12
PRINT "Type values for the following system variables:" : PRINT
IF COMP$="Yes" THEN GOTO 611 ELSE GOTO 612
611 PRINT " Pressure, psia";" ( 1400 < Range < 2700 )"
GOTO 613
612 PRINT " Pressure, psia";" ( Hot Leg P sat < Range < 3200 )"
613 PRINT
PRINT TAB(A%); : INPUT "Initial Value: ";PRES.I
PRINT TAB(A%); : INPUT "Final Value : ";PRES.F

```

```

PRINT "establish the density of the leakage. The choices"
PRINT "are:" : PRINT
PRINT " (A) Standard Conditions,"
PRINT " (B) Average Reactor Cooling System Conditions,"
PRINT " (C) Other." : PRINT
INPUT "Which would you like (A/B/C)? ";X$

IF X$="A" THEN LEAK.COND$="Standard" : LEAK.TEMP=70 : \
LEAK.PRES=14.7 : GOTO 630
IF X$="B" THEN LEAK.COND$="Ave RCS" : \
LEAK.TEMP=(T.AVE.I+T.AVE.F)/2 : \
LEAK.PRES=(PRES.I+PRES.F)/2 : GOTO 630
IF X$="C" THEN LEAK.COND$="Other" : PRINT : PRINT : PRINT \
: GOTO 624 ELSE GOTO 623
624 INPUT "Type the selected temperature in degrees F: ";LEAK.TEMP
INPUT "Type the selected pressure in psia: ";LEAK.PRES

630 \
** CALCULATIONS **

\References:
\ (1) "ASME Steam Tables," Fourth Edition.
\ (2) "Horizontal Tanks," Note to J. Chung from R. Woodruff,
\ May 22, 1981.

IF COMP$="No" THEN GOTO 640 ELSE GOTO 641

640 \
* Uncompensated Pressurizer *

PZR.INV.I = PZR.SLOPE * PZR.LVL.I
PZR.INV.F = PZR.SLOPE * PZR.LVL.F

GOTO 642

641 \
* Compensated Pressurizer *

PRES = RES.I : GOSUB 840 REM: Saturation Temperature
TEMP = TEMP.SAT : GOSUB 850 REM: Density of water
GOSUB 860 REM: Density of Saturated Steam

PZR.INV.I = DENSITY.WTR * PZR.BTM.VOL + DENSITY.STM \
* PZR.TOP.VOL + (DENSITY.WTR - DENSITY.STM) \
* (PZR.LVL.I - PZR.LVL.NOM) * PZR.SLOPE

PRES = PRES.F : GOSUB 840
TEMP = TEMP.SAT : GOSUB 850
GOSUB 860

```

```

\          * Water Charged and Drained *
MASS.CHARGED = 9.3238 * GAL.CHARGED : REM: Mass in Pounds
MASS.DRAINED = 8.3238 * GAL.DRAINED

```

```

\          * Leakage Density *
PRES = LEAK.PRES : TEMP = LEAK.TEMP
GOSUB 850 : REM Density of Water
LEAK.DENSITY = DENSITY.WTR

```

```

\          * Leak Rates *
RCS.INV.CHG = UP.INV.CHG + PZR.INV.CHG + LDT.INV.CHG \
- MASS.CHARGED + MASS.DRAINED
GROSS.LEAK.RATE = -RCS.INV.CHG/LEAK.DENSITY*7.481/DURATION/60
IDENT.LEAK.RATE = (RQT.INV.CHG + D1.INV.CHG)/LEAK.DENSITY \
*7.481/DURATION/60
UNIDENT.LEAK.RATE = GROSS.LEAK.RATE - IDENT.LEAK.RATE

```

```

690 \          ** DATA OUTPUT **
IF PRINT.FLAG$="Y" THEN LPRINTER
PRINT : PRINT : PRINT TAB(39);"NRC" : PRINT
PRINT TAB(24);"INDEPENDENT MEASUREMENTS PROGRAM"
PRINT
PRINT TAB(24);"REACTOR COOLING SYSTEM LEAK RATES"
PRINT : PRINT
PRINT TAB(11);"STATION: ";PLANT$;TAB(44);"TEST DATE : ";
PRINT DATE$
PRINT TAB(11);"UNIT : ";UNIT$;TAB(44);"START TIME: ";
PRINT TIME$
PRINT TAB(11);"DOCKET : 50-";DOCKET$;TAB(44);
PRINT "DURATION :";DURATION;"hours" : PRINT : PRINT
GOSUB 900 REM: Conditional Stop
PRINT TAB(36);"TEST DATA" : PRINT
PRINT TAB(48);"Initial";TAB(63);"Final"
PRINT TAB(16);"System Parameters:" : PRINT
PRINT TAB(17);"Pressure psia";TAB(48);PRES.I;TAB(62);PRES.F
PRINT TAB(17);"T Ave, degrees F";TAB(48);T.AVE.I;TAB(62);
PRINT T.AVE.F : PRINT
PRINT TAB(16);"Water Levels:" : PRINT
PRINT TAB(17);"Pressurizer, ";PZR.UNITS$;TAB(48);
PRINT PZR.LUL.I;TAB(62);PZR.LUL.F

```

```

PRINT USING "##.##";GROSS.LEAK.RATE;
PRINT TAB(30);"Identified";Tab(46);
PRINT USING "##.##";IDENT.LEAK.RATE
PRINT TAB(30);"Unidentified";Tab(46);
PRINT USING "##.##";UNIDENT.LEAK.RATE
PRINT : PRINT

PRINT TAB(11);"(1) Determined from tank calibration curve."
PRINT TAB(11);"(2) Determined from tank dimensions."
PRINT TAB(11);"(3) The density used for converting inventory ";
PRINT "change to leak" : PRINT TAB(16);"rate was ";
PRINT USING "##.##";LEAK.DENSITY;
PRINT " pounds/cubic foot based on";
IF LEAK.CONDS="Standard" THEN PRINT " standard"
IF LEAK.CONDS="Ave RCS" THEN PRINT " average RCS"
IF LEAK.CONDS="Standard" OR LEAK.CONDS="Ave RCS" THEN PRINT \
  TAB(16);"conditions."
IF LEAK.CONDS="Other" THEN PRINT LEAK.TEMP;"degrees F and"
IF LEAK.CONDS="Other" THEN PRINT TAB(16);"and";LEAK.PRES;"psia."
GOSUB 900 REM: Conditional Stop

699 CONSOLE : CLOSE 2 : GOTO 995

\
      ** ANALYTICAL SUBROUTINES **

840 \
      * Saturation Temperature *

\Note: This calculation is based on Page 17, Section 5,
\ Reduced saturation pressure, of Reference (1). It
\ duplicates saturation temperature as given in Table 2 of
\ Reference (1) for pressures from 14.696 psia to 3208.2 psia.

BETA = PRES*9.80665*0.45359237/22120000/0.0254/0.0254

PRINT : PRINT : PRINT
PRINT "      Calculating Saturation Temperature"
PRINT "      for ";PRES;"psia"

THETA = 0.5 : THETA1 = 0.25

841 SK1 =-7.691234564      : SK2 =-2.608023696E+1
SK3 =-1.681706546E+2     : SK4 = 6.423285504E+1
SK5 =-1.189646225E+2     : SK6 = 4.16711732
SK7 = 2.09750676E+1      : SK8 = 1E9
SK9 = 6

T1 = 1-THETA : T2 = T1*T1 : T3 = T1*T2 : T4 = T1*T3
T5 = T1*T4

BETA1 = EXP(1/THETA*(SK1*T1+SK2*T2+SK3*T3+SK4*T4+SK5*T5) \
  /(1+SK6*T1+SK7*T2)-T1/(SK8*T2+SK9))

```


BETA = PRES*9.80665*0.45359237/22120000/0.0254/0.0254
 BETA2 = BETA*BETA : BETA3 = BETA*BETA2

Y = 1-SA1*THETA2-SA2/THETA6

Z = Y+SQR(SA3*Y*Y-2*SA4*THETA+2*SA5*BETA)

CHI1 = A11*SA5/EXP(LOG(Z)*5/17) + (A12+A13*THETA+A14*THETA2 \\
 + A15*EXP(LOG(ABS(SA6-THETA))*10)+A16/(SA7+THETA19)) \\
 - 1/(SA8+THETA11)*(A17+2*A18*BETA+3*A19*BETA2) \\
 - A20*THETA18*(SA9+THETA2)*(-3/EXP(LOG(SA10+BETA))*4)+SA11) \\
 + 3*A21*(SA12-THETA)*BETA2 + 4*A22/THETA20*BETA3

SPECIFIC.VOL=CHI1*3.17*0.0160184634

DENSITY.WTR = 1/SPECIFIC.VOL : RETURN REM: 1b/ft3

860 \ * Density of Saturated Steam *

\ Note: The following equation is a curve fit to the density of
 \ saturated steam as given on pages 90 and 91 of Reference (1).
 \ It is accurate to 1.0% or better in the range from 1400 to
 \ 2700 psia.

PRINT : PRINT : PRINT
 PRINT * Calculating the Density of Saturated"
 PRINT * Steam at ";PRES;"psia"

P = PRES-2000

DENSITY.STM = 5.3104+3.8887E-3*P+1.2782E-6*P*P+6.24E-10*P*P*P

RETURN

\ * Tank Inventory *

865 \ Calibration Method

INV.CHG = SLOPE * (LVL.F - LVL.I) : RETURN

870 \ Geometric Method

IF CVX.RAD<CYL.RAD THEN CONSOLE : PRINT : PRINT : PRINT \\
 : PRINT "ERROR: Radius of Convex Head is less than" \\
 : PRINT "Radius of Tank." : GOTO 995

IF UNITS\$="inches" THEN LVL.FRAC.I=LVL.I/12/2/CYL.RAD \\
 ELSE LVL.FRAC.I=LVL.I/100

IF UNITS\$="inches" THEN LVL.FRAC.F=LVL.F/12/2/CYL.RAD \\
 ELSE LVL.FRAC.F=LVL.F/100

890

```

*****
* PLANT PARAMETERS FILE *
*****

```

```

READ #2, 1; PLANT$           : READ #2, 2; UNIT$
READ #2, 3; NSSS$           : READ #2, 4; VP.VOL
READ #2, 5; PZR.UNITS$      : READ #2, 6; COMP$
READ #2, 7; PZR.LVL.NQM     : READ #2, 8; PZR.BTM.VOL
READ #2, 9; PZR.TOP.VOL     : READ #2,10; FZR.SLOPE
READ #2,11; PZR.UP.LMT      : READ #2,12; PZR.LO.LMT
READ #2,13; LD.TANK$        : READ #2,14; LDT.UNITS$
READ #2,15; LDT.SLOPE       : READ #2,16; LDT.UP.LMT
READ #2,17; LDT.LO.LMT      : READ #2,18; LDT.GEO$
READ #2,19; LDT.CYL.RAD     : READ #2,20; LDT.CYL.LEN
READ #2,21; LDT.CUX.RAD     : READ #2,22; LDT.DENSITY
READ #2,23; LDT.NORMFAC     : READ #2,24; DT.UNITS$
READ #2,25; DT.SLOPE        : READ #2,26; DT.UP.LMT
READ #2,27; DT.LO.LMT       : READ #2,28; DT.GEO$
READ #2,29; DT.CYL.RAD      : READ #2,30; DT.CYL.LEN
READ #2,31; DT.CUX.RAD      : READ #2,32; DT.DENSITY
READ #2,33; DT.NORMFAC      : READ #2,34; RQ.TANK$
READ #2,35; RQT.UNITS$      : READ #2,36; RQT.SLOPE
READ #2,37; RQT.UP.LMT      : READ #2,38; RQT.LO.LMT
READ #2,39; RQT.GEO$        : READ #2,40; RQT.CYL.RAD
READ #2,41; RQT.CYL.LEN     : READ #2,42; RQT.CUX.RAD
READ #2,43; RQT.DENSITY     : READ #2,44; RQT.NORMFAC
READ #2,45; DOCKET$         : RETURN

```

```
995 \
\
\
*****
* CONTINUATION OR TERMINATION *
*****

CONSOLE : PRINT : PRINT : PRINT
INPUT "Do you wish to terminate this session (Y/N)?";X$
IF X$(">"Y" AND X$(">"N" THEN GOTO 995
IF X$ = "N" THEN GOTO 1 ELSE GOTO 999
999 PRINT : PRINT : PRINT : STOP
END
```

AUTOST.COM


```

0100 2A 01 00 2E 00 7C D6 16 *....!..
0108 67 22 65 01 11 20 03 01 g"e... ..
0110 FF 07 1A D6 41 12 13 08 ....A...
0118 78 B7 C2 12 01 11 73 01 x.....s.
0120 CD 60 01 11 00 F0 21 20 .\.....!
0128 03 01 00 07 ED B0 11 75 .....u
0130 01 CD 60 01 11 67 01 01 ..\
0138 0A 00 2A 65 01 2E 07 CD ..*.....
0140 55 01 2A 65 01 2E 88 3E U.*e...>
0148 08 77 2A 65 01 2E 89 7C .w*e...!
0150 77 2A 65 01 E9 1A 77 23 w*e...w#
0158 13 08 78 B1 C2 55 01 C9 ..x...U..
0160 0E 09 C3 05 00 00 34 04 .....4.
0168 43 52 55 4E 32 20 48 00 CRUN2 H.
0170 00 00 00 1A 24 1B 3D 30 .....$.=0
0178 21 20 20 20 20 20 20 20 !
0180 20 20 20 20 20 20 20 20
0188 20 20 20 20 20 20 20 20
0190 20 20 20 20 20 20 20 20
0198 20 20 20 20 20 20 20 20
01A0 20 20 20 20 20 20 20 20
01A8 20 20 20 20 0D 0A 20 20 ..
01B0 20 20 20 20 20 20 20 20
01B8 20 20 20 49 4E 44 45 50 INDEP
01C0 45 4E 44 45 4E 54 20 4D ENDENT M
01C8 45 41 53 55 52 45 4D 45 EASUREME
01D0 4E 54 53 20 20 20 20 20 NTS
01D8 20 20 20 20 20 20 20 20
01E0 20 0D 0A 20 20 20 20 20 ..
01E8 20 20 20 20 20 20 20 20
01F0 20 20 20 20 20 20 20 20
01F8 50 52 4F 47 52 41 4D 20 PROGRAM
0200 20 20 20 20 20 20 20 20
0208 20 20 20 20 20 20 20 20
0210 20 20 20 20 20 20 0D 0A ..
0218 20 20 20 20 20 20 20 20
0220 20 20 20 20 20 20 20 20
0228 20 20 20 20 20 20 20 20
0230 20 20 20 20 20 20 20 20
0238 20 20 20 20 20 20 20 20
0240 20 20 20 20 20 20 20 20
0248 20 20 20 0D 0A 20 20 20 ..
0250 20 20 20 20 20 55 2E 53 U.S
0258 2E 20 4E 75 63 6C 65 61 . Nuclea
0260 72 20 52 65 67 75 6C 61 r Regula
0268 74 6F 72 79 20 43 6F 6D tory Com
0270 6D 69 73 73 69 6F 6E 20 mission
0278 20 20 20 20 20 20 20 20
0280 0D 0A 20 20 20 20 20 20 ..
0288 20 20 20 20 20 20 20 20
0290 57 61 73 68 69 6E 67 74 Washingt
0298 6F 6E 2C 20 44 43 20 20 on, DC

```

0450	61	61	61	61	61	61	61	61	aaaaaaaa
0458	61	61	61	61	61	61	61	61	aaaaaaaa
0460	61	61	61	61	61	61	61	61	aaaaaaaa
0468	61	61	61	61	61	61	61	61	aaaaaaaa
0470	61	61	61	61	61	61	61	61	aaaaaaaa
0478	61	61	61	61	61	61	61	61	aaaaaaaa
0480	61	61	61	61	61	61	61	61	aaaaaaaa
0488	61	61	61	61	61	61	61	61	aaaaaaaa
0490	61	61	61	61	61	61	61	61	aaaaaaaa
0498	61	61	61	61	61	61	61	61	aaaaaaaa
04A0	61	61	61	61	61	61	61	61	aaaaaaaa
04A8	61	61	61	61	61	61	61	61	aaaaaaaa
04B0	61	61	61	61	61	61	61	61	aaaaaaaa
04B8	61	61	61	61	61	61	61	61	aaaaaaaa
04C0	61	61	61	61	61	61	61	61	aaaaaaaa
04C8	61	61	61	61	61	61	61	61	aaaaaaaa
04D0	61	61	61	61	61	61	61	61	aaaaaaaa
04D8	61	61	61	61	61	61	61	61	aaaaaaaa
04E0	61	61	61	61	61	61	61	61	aaaaaaaa
04E8	61	61	61	61	61	61	61	61	aaaaaaaa
04F0	61	61	61	61	61	61	61	61	aaaaaaaa
04F8	61	61	61	61	61	61	61	61	aaaaaaaa
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0508	61	61	61	61	61	61	61	61	aaaaaaaa
0510	61	61	61	61	61	61	61	61	aaaaaaaa
0518	61	61	61	61	61	61	61	61	aaaaaaaa
0520	59	59	59	59	59	59	59	59	YYYYYYYY
0528	59	59	59	59	59	59	59	59	YYYYYYYY
0530	59	59	59	59	59	59	59	59	YYYYYYYY
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0568	61	61	61	61	61	61	61	61	aaaaaaaa
0570	61	61	61	61	61	61	61	61	aaaaaaaa
0578	41	61	42	61	43	61	44	61	AaBaCaDa
0580	45	61	46	61	47	61	48	61	EaFaGaHa
0588	49	61	4A	61	4B	61	4C	61	IaJaKaLa
0590	4D	61	4E	61	4F	61	50	61	MaNaOaPa
0598	51	61	52	61	53	61	54	61	QaRaSaTa
05A0	57	61	61	61	61	61	61	61	Waaaaaaaa
05A8	61	61	61	61	61	61	61	61	aaaaaaaa
05B0	61	61	61	61	61	61	61	61	aaaaaaaa
05B8	61	61	61	61	61	61	61	61	aaaaaaaa
05C0	61	61	61	61	61	61	61	61	aaaaaaaa
05C8	61	61	61	61	61	61	61	61	aaaaaaaa
05D0	61	61	57	61	61	61	61	61	aaWaaaaa
05D8	61	61	61	61	61	61	61	61	aaaaaaaa
05E0	61	61	61	61	61	61	61	61	aaaaaaaa
05E8	61	61	61	61	61	61	61	61	aaaaaaaa

07A0	57	61	61	61	61	61	61	61	Waaaaaaaa
07A8	61	61	61	61	61	57	61	61	aaaaaWaa
07B0	56	49	57	61	61	61	57	61	VIWaaaWa
07B8	61	61	56	49	61	61	61	57	aaVIaaaW
07C0	61	61	61	61	59	61	61	61	aaaaYaaa
07C8	61	61	61	61	61	61	61	61	aaaaaaaaa
07D0	61	61	57	61	61	61	61	61	aaWaaaaa
07D8	61	61	61	61	61	61	61	61	aaaaaaaaa
07E0	61	61	61	61	61	61	61	61	aaaaaaaaa
07E8	61	61	61	61	61	61	61	61	aaaaaaaaa
07F0	61	61	61	61	61	61	61	61	aaaaaaaaa
07F8	61	61	61	61	61	61	61	61	aaaaaaaaa
0800	61	61	61	61	61	61	61	61	aaaaaaaaa
0808	61	61	61	61	61	61	61	61	aaaaaaaaa
0810	61	61	61	61	61	61	61	61	aaaaaaaaa
0818	61	61	61	61	61	61	61	61	aaaaaaaaa
0820	57	61	61	61	61	61	61	61	Waaaaaaaa
0828	61	61	61	61	61	57	61	61	aaaaaWaa
0830	61	56	57	61	61	61	57	61	aVWaaaWa
0838	61	61	61	56	49	61	61	57	aaaVIaaw
0840	59	59	59	59	57	61	61	61	YYYYWaaa
0848	61	61	61	61	61	61	61	61	aaaaaaaaa
0850	61	61	57	61	61	61	61	61	aaWaaaaa
0858	61	61	61	61	61	61	61	61	aaaaaaaaa
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0868	61	61	61	61	61	61	61	61	aaaaaaaaa
0870	61	61	61	61	61	61	61	61	aaaaaaaaa
0878	61	61	61	61	61	61	61	61	aaaaaaaaa
0880	61	61	61	61	61	61	61	61	aaaaaaaaa
0888	61	61	61	61	61	61	61	61	aaaaaaaaa
0890	61	61	61	61	61	61	61	61	aaaaaaaaa
0898	61	61	61	61	61	61	61	61	aaaaaaaaa
08A0	57	61	61	61	61	61	61	61	Waaaaaaaa
08A8	61	61	61	61	61	61	61	61	aaaaaaaaa
08B0	61	61	61	61	61	61	61	61	aaaaaaaaa
08B8	61	61	61	61	61	61	61	61	aaaaaaaaa
08C0	61	61	61	61	61	61	61	61	aaaaaaaaa
08C8	61	61	61	61	61	61	61	61	aaaaaaaaa
08D0	61	61	57	61	61	61	61	61	aaWaaaaa
08D8	61	61	61	61	61	61	61	61	aaaaaaaaa
08E0	61	61	61	61	61	61	61	61	aaaaaaaaa
08E8	61	61	61	61	61	61	61	61	aaaaaaaaa
08F0	61	61	61	61	61	61	61	61	aaaaaaaaa
08F8	61	61	61	61	61	61	61	61	aaaaaaaaa
0900	61	61	61	61	61	61	61	61	aaaaaaaaa
0908	61	61	61	61	61	61	61	61	aaaaaaaaa
0910	61	61	61	61	61	61	61	61	aaaaaaaaa
0918	61	61	61	61	61	61	61	61	aaaaaaaaa
0920	57	59	59	59	59	59	59	59	WYYYYYYY
0928	59	59	59	59	59	59	59	59	YYYYYYYY
0930	59	59	59	59	59	59	59	59	YYYYYYYY
0938	59	59	59	59	59	59	59	59	YYYYYYYY
0940	59	59	59	59	59	59	59	59	YYYYYYYY
0948	59	59	59	59	59	59	59	59	YYYYYYYY

APPENDIX C

H.BAS

**** H.BAS ****

\H.INT is executed by AUTOST.COM.

%CHAIN 500,21700,0,1700
CHAIN "RCSLK8"
END

PARTIAL TANK VOLUMES

PARTIAL TANK VOLUMES

As suggested by J. W. Chung, the volume of water, V , in a partially-filled, horizontal tank with convex heads can be calculated by integrating Sdh where S is the surface area and dh is the thickness of a horizontal, incremental slab of water located at height h above the bottom of the tank.

The surface of the slab has the shape and dimensions shown in Figure 1. The area of the surface can be calculated by dividing it into a rectangle and two circular segments. The area of the rectangle is $2cL$ and the combined area of the two circular segments is $bbB - ac$ where angle B is expressed in radians and is equal to $\arctan(c/a)$. Term bbB is twice the area of the smallest circular sector containing one of the segments, and term ac is twice the area of the largest isosceles triangle contained in the sector.

The volume of the incremental slab is

$$dV = [2cL + bb \arctan(c/a) - ac] dh$$

Before this expression can be integrated, a , b , and c must be expressed in terms of h and the tank dimensions, R , H , and L , where R and H are the radii of the cylindrical part of the tank and the heads and L is the length of the cylindrical part of the tank. The relationships between R , H , L , and h and the dimensions of the incremental slab surface are shown in Figure 2.

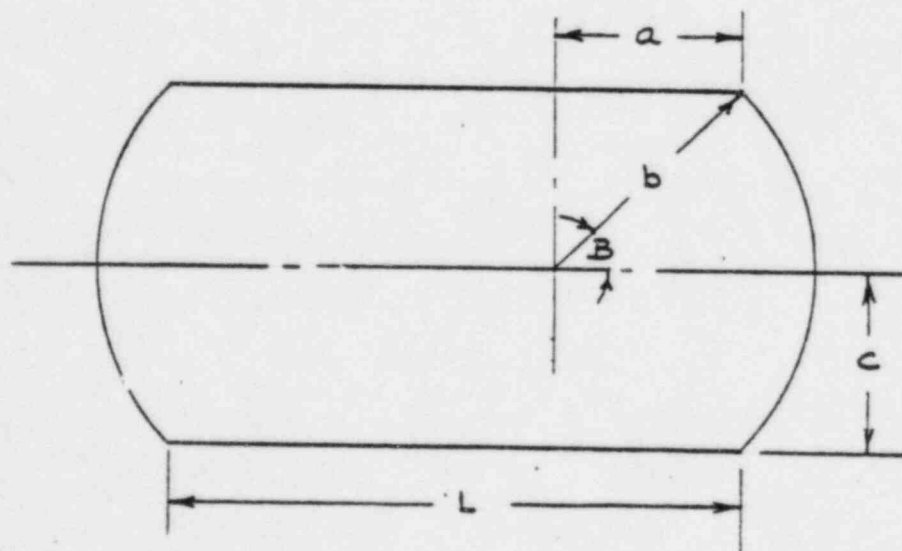


Figure 1: Slab Surface

This expression for dV is the basis for the numerical integration in the Tank Inventory Subroutine using the geometric method which is given on pages A-27 and 28 of Appendix A. In the subroutine, the height increment is set at 1% or less of the tank diameter and the surface area is the mean of the upper and lower surfaces of the slab. Slab volumes are calculated and summed from the initial surface level to the final surface level.

CURRENT PLANT LIST

PLANTS WITH PARAMETERS FILED

50-255	Palisades 1
50-266	Point Beach 1
50-282	Prairie Island 1
50-295	Zion 1
50-301	Point Beach 2
50-304	Zion 2
50-305	Kewaunee 1
50-306	Prairie Island 2
50-312	Rancho Seco 1
50-315	D. C. Cook 1
50-316	D. C. Cook 2
50-317	Calvert Cliffs 1
50-318	Calvert Cliffs 2
50-320	Three Mile Island 2
50-344	Trojan 1
50-346	Davis Besse 1
50-348	Farley 1

CURRENT PARAMETER LISTS

APPENDIX F: CURRENT PLANT LIST

PARAMETER LIST

Unit Identification:	
Plant Name	Calvert Cliffs
Unit Number	1
Docket Number	50-317
Nuclear Steam System Supplier	Combustion Engineering
Vessel and Piping:	
Volume	9601 cubic feet
Pressurizer:	
Level Units	inches
Temperature Compensated Calibration Curve	No
Slope	139.82 pounds per inch
Upper Level Limit	375 inches
Lower Level Limit	32 inches
Relief	Quench Tank
Volume Control Tank:	
Level Units	inches
Calibration Curve	
Slope	230.389 pounds per inch
Upper Level Limit	168 inches
Lower level limit	0 inches
Geometric Method Available	No
Drain Tank:	
Level Units	inches
Calibration Curve	
Slope	174.513 pounds per inch
Upper Level Limit	40 inches
Lower level limit	15 inches
Water Density	62.27 pounds per cubic foot
Geometric Method Available	Yes
Dimensions	
Cylinder Radius	2.2422 feet
Cylinder Length	7.2292 feet
Head Radius	4.4844 feet
Normalization Factor	0.9755
Quench Tank:	
Level Units	inches
Calibration Curve	
Slope	291.513 pounds per inch
Upper Level Limit	40 inches
Lower level limit	15 inches
Water Density	62.27 pounds per cubic foot
Geometric Method Available	Yes
Dimensions	
Cylinder Radius	2.474 feet
Cylinder Length	10.494 feet
Head Radius	4.4459 feet
Normalization Factor	1.0254

PARAMETER LIST

Unit Identification:	
Plant Name	D. C. Cook
Unit Number	1
Docket Number	50-315
Nuclear Steam System Supplier	Westinghouse
Vessel and Piping:	
Volume	10812 cubic feet
Pressurizer:	
Level Units	%
Temperature Compensated	No
Calibration Curve	
Slope	579.367 pounds per %
Upper Level Limit	100 %
Lower level Limit	0 %
Relief	Relief Tank
Volume Control Tank:	
Level Units	%
Calibration Curve	
Slope	161.619 pounds per %
Upper Level Limit	100 %
Lower level limit	0 %
Geometric Method Available	No
Drain Tank:	
Level Units	%
Calibration Curve	
Slope	30.144 pounds per %
Upper Level Limit	75 %
Lower level limit	25 %
Geometric Method Available	No
Relief Tank:	
Level Units	%
Calibration Curve	
Slope	1209.88 pounds per %
Upper Level Limit	80 %
Lower level limit	20 %
Geometric Method Available	No

PARAMETER LIST

Unit Identification:	
Plant Name	Davis Besse
Unit Number	1
Docket Number	50-346
Nuclear Steam System Supplier	Babcock & Wilcox
Vessel and Piping:	
Volume	10040 cubic feet
Pressurizer:	
Level Units	inches
Temperature Compensated	Yes
Nominal Level	200 inches
Volume Below Nominal Level	681.87 cubic feet
Volume Above Nominal Level	0 cubic feet
Calibration Curve	
Slope	3.1863 cubic feet per inch
Upper Level Limit	456 inches
Lower level Limit	48 inches
Relief	Relief Tank
Makeup Tank:	
Level Units	inches
Calibration Curve	
Slope	258.221 pounds per inch
Upper Level Limit	100 inches
Lower level limit	0 inches
Geometric Method Available	No
Drain Tank:	
Level Units	inches
Calibration Curve	
Slope	62.473 pounds per inch
Upper Level Limit	80 inches
Lower level limit	15 inches
Geometric Method Available	No
Relief Tank:	
Level Units	inches
Calibration Curve	
Slope	368.034 pounds per inch
Upper Level Limit	120 inches
Lower level limit	48 inches
Geometric Method Available	No

PARAMETER LIST

Unit Identification:	
Plant Name	Kewaunee
Unit Number	1
Docket Number	50-305
Nuclear Steam System Supplier	Westinghouse
Vessel and Piping:	
Volume	5591 cubic feet
Pressurizer:	
Level Units	%
Temperature Compensated	No
Calibration Curve	
Slope	327.8 pounds per %
Upper Level Limit	100 %
Lower level Limit	0 %
Relief	Relief Tank
Volume Control Tanks:	
Level Units	%
Calibration Curve	
Slope	105.6 pounds per %
Upper Level Limit	100 %
Lower level limit	0 %
Geometric Method Available	No
Drain Tank:	
Level Units	%
Calibration Curve	
Slope	29.33 pounds per %
Upper Level Limit	80 %
Lower level limit	20 %
Geometric Method Available	No
Relief Tank:	
Level Units	%
Calibration Curve	
Slope	557.74 pounds per %
Upper Level Limit	74 %
Lower level limit	72 %
Geometric Method Available	No

PARAMETER LIST

Unit Identification:	
Plant Name	Point Beach
Unit Number	1
Docket Number	50-266
Nuclear Steam System Supplier	Westinghouse
Vessel and Piping:	
Volume	5440 cubic feet
Pressurizer:	
Level Units	%
Temperature Compensated	Yes
Nominal Level	50 %
Volume Below Nominal Level	500 cubic feet
Volume Above Nominal Level	0 cubic feet
Calibration Curve	
Slope	8.56 cubic feet per %
Upper Level Limit	61 %
Lower level Limit	38 %
Relief	Relief Tank
Volume Control Tanks:	
Level Units	%
Calibration Curve	
Slope	107.25 pounds per %
Upper Level Limit	78 %
Lower level limit	8 %
Geometric Method Available	No
Drain Tanks:	
Level Units	%
Calibration Curve	
Slope	33.27 pounds per %
Upper Level Limit	50 %
Lower level limit	7 %
Geometric Method Available	No
Relief Tank:	
Level Units	%
Calibration Curve	
Slope	519.89 pounds per %
Upper Level Limit	76 %
Lower level limit	66 %
Geometric Method Available	No

PARAMETER LIST

Unit Identification:	
Plant Name	Prairie Island
Unit Number	1
Docket Number	50-282
Nuclear Steam System Supplier	Westinghouse
Vessel and Piping:	
Volume	5591 cubic feet
Pressurizer:	
Level Units	%
Temperature Compensated	Yes
Nominal Level	35 %
Volume Below Nominal Level	372.944 cubic feet
Volume Above Nominal Level	0 cubic feet
Calibration Curve	
Slope	8.637 cubic feet per %
Upper Level Limit	100 %
Lower level Limit	0 %
Relief	Relief Tank
Volume Control Tank:	
Level Units	%
Calibration Curve	
Slope	104.954 pounds per %
Upper Level Limit	100 %
Lower level limit	0 %
Geometric Method Available	No
Drain Tank:	
Level Units	%
Calibration Curve	
Slope	28.599 pounds per %
Upper Level Limit	80 %
Lower level limit	20 %
Geometric Method Available	No
Relief Tank:	
Level Units	%
Calibration Curve	
Slope	527.548 pounds per %
Upper Level Limit	80 %
Lower level limit	20 %
Geometric Method Available	No

PARAMETER LIST

Unit Identification:

Plant Name	Rancho Seco
Unit Number	1
Docket Number	50-312
Nuclear Steam System Supplier	Babcock & Wilcox

Vessel and Piping:

Volume	10578.2 cubic feet
--------	--------------------

Pressurizer:

Level Units	inches
Temperature Compensated	Yes
Nominal Level	200 inches
Volume Below Nominal Level	872.6 cubic feet
Volume Above Nominal Level	0 cubic feet
Calibration Curve	
Slope	3.16678 cubic feet per inch
Upper Level Limit	320 inches
Lower level Limit	0 inches
Relief	Drain Tank

Makeup Tanks:

Level Units	inches
Calibration Curve	
Slope	256 pounds per inch
Upper Level Limit	100 inches
Lower level limit	0 inches
Geometric Method Available	No

Drain Tanks:

Level Units	inches
Calibration Curve	
Slope	280 pounds per inch
Upper Level Limit	120 inches
Lower level limit	48 inches
Geometric Method Available	No

APPENDIX F: CURRENT PLANT LIST

PARAMETER LIST

Unit Identification:	
Plant Name	Trojan
Unit Number	1
Docket Number	50-344
Nuclear Steam System Supplier	Westinghouse
Vessel and Piping:	
Volume	10811 cubic feet
Pressurizer:	
Level Units	%
Temperature Compensated Calibration Curve	No
Slope	1215 pounds per %
Upper Level Limit	100 %
Lower level Limit	0 %
Relief	Relief Tank
Volume Control Tank:	
Level Units	%
Calibration Curve	
Slope	158.9 pounds per %
Upper Level Limit	100 %
Lower level limit	40 %
Geometric Method Available	No
Drain Tank:	
Level Units	%
Calibration Curve	
Slope	33.7 pounds per %
Upper Level Limit	70 %
Lower level limit	20 %
Water Density	62.27 pounds per cubic foot
Geometric Method Available	Yes
Dimensions	
Cylinder Radius	1.4821 feet
Cylinder Length	6.2756 feet
Head Radius	2.1695 feet
Normalization Factor	0.9234
Relief Tank:	
Level Units	%
Calibration Curve	
Slope	1176 pounds per %
Upper Level Limit	70 %
Lower level limit	30 %
Water Density	62.27 pounds per cubic foot
Geometric Method Available	Yes
Dimensions	
Cylinder Radius	4.75 feet
Cylinder Length	23.315 feet
Head Radius	6.5276 feet
Normalization Factor	0.8269

PARAMETER LIST

Unit Identifications:	
Plant Name	Zion
Unit Number	2
Docket Number	50-304
Nuclear Steam System Supplier	Westinghouse
Vessel and Piping:	
Volume	10938 cubic feet
Pressurizer:	
Level Units	%
Temperature Compensated	No
Calibration Curve	
Slope	597.59 pounds per %
Upper Level Limit	100 %
Lower level Limit	0 %
Relief	Relief Tank
Volume Control Tank:	
Level Units	%
Calibration Curve	
Slope	159.95 pounds per %
Upper Level Limit	100 %
Lower level limit	0 %
Geometric Method Available	No
Drain Tank:	
Level Units	%
Calibration Curve	
Slope	29.75 pounds per %
Upper Level Limit	90 %
Lower level limit	10 %
Geometric Method Available	No
Relief Tank:	
Level Units	%
Calibration Curve	
Slope	1205.62 pounds per %
Upper Level Limit	80 %
Lower level limit	20 %
Geometric Method Available	No

EXAMPLES

NRC

INDEPENDENT MEASUREMENTS PROGRAM
REACTOR COOLING SYSTEM LEAK RATESSTATION: Calvert Cliffs
UNIT : 1
DOCKET : 50-317TEST DATE : March 18, 1983
START TIME: Software Test
DURATION : 2 hours

TEST DATA

System Parameters:	Initial:	Final
Pressure, psia	2140	2135
T Ave, degrees F	581	582
Water Levels:		
Pressurizer, inches	43	44
Quench Tank, inches	30	31
Volume Control Tank, inches	60	59
Drain Tank, inches	21	22

Water Charged = 10 gal

Water Drained = 2 gal

TEST RESULTS

Change in Water Inventory in pounds:

Vessel & Piping	-785	Quench Tank (1)	292
Pressurizer	140	Drain Tank (1)	175
Volume Control Tank (1)	-230		
Less: Water Charged	83	Collected Leakage	<u>466</u>
Plus: Water Drained	17		
Cooling System	<u>-943</u>		

Leak Rates in gpm (3):

Gross	0.94
Identified	0.47
Unidentified	0.48

- (1) Determined from tank calibration curve.
 (2) Determined from tank dimensions.
 (3) The density used for converting inventory change to leak rate was 62.31 pounds/cubic foot based on standard conditions.

NRC

INDEPENDENT MEASUREMENTS PROGRAM
 REACTOR COOLING SYSTEM LEAK RATES

STATION: Farley
 UNIT : 1
 DOCKET : 50-348

TEST DATE : March 18, 1983
 START TIME: Software Test
 DURATION : 2 hours

TEST DATA

	Initial	Final
System Parameters:		
Pressure, psia	2138	2128
T Ave, degrees F	581	582
Water Levels:		
Pressurizer, %	44	43
Relief Tank, %	70	71
Volume Control Tank, %	60	59
Drain Tank, %	21	22
Water Charged = 10 gal		Water Drained = 2 gal

TEST RESULTS

Change in Water Inventory in pounds:

Vessel & Piping	-718	Relief Tank (1)	830
Pressurizer	-396	Drain Tank (1)	32
Volume Control Tank (1)	-115		
Less: Water Charged	83	Collected Leakage	<u>862</u>
Plus: Water Drained	17		
Cooling System	<u>-1295</u>		

Leak Rates in gpm (3):

Gross	1.30
Identified	0.86
Unidentified	0.43

- (1) Determined from tank calibration curve.
 (2) Determined from tank dimensions.
 (3) The density used for converting inventory change to leak rate was 62.31 pounds/cubic foot based on standard conditions.

NRC

INDEPENDENT MEASUREMENTS PROGRAM
 REACTOR COOLING SYSTEM LEAK RATES

STATION: Three Mile Island
 UNIT : 2
 DOCKET : 50-320

TEST DATE : March 18, 1983
 START TIME: Software Test
 DURATION : 4 hours

TEST DATA

System Parameters:	Initial	Final
Pressure, psia	2100	2000
T Ave, degrees F	570	580
Water Levels:		
Pressurizer, inches	230	220
Makeup Tank, inches	60	70
Drain Tank, inches	73	80
Water Charged = 100 gal		Water Drained = 0 gal

TEST RESULTS

Change in Water Inventory in pounds:

Vessel & Piping	-8669	Drain Tank (1)	4276
Pressurizer	-648		
Makeup Tank (1)	2570		
Less: Water Charged	832		
Plus: Water Drained	0		
Cooling System	<u>-7579</u>		

Leak Rates in gpm (3):

Gross	3.79
Identified	2.14
Unidentified	1.65

- (1) Determined from tank calibration curve.
 (2) Determined from tank dimensions.
 (3) The density used for converting inventory change to leak rate was 62.31 pounds/cubic foot based on standard conditions.

K-12

Notes on Discussion w J F Lloyd.

3/31/80

Talked w Floyd:

Said believed correction to RC leakage test made after RC DT Pump out during test showed error in computer code.

The only time the RC DT was ever pumped out during RC test.

Wrote 3/14/79 temporary procedure change was approved by PORC on 3/16/79 and used for the first time on 20-09 the same day.

Floyd said that controlled leakage included 2nd and 3rd seal leakage.

2nd seal leakage measured by computer on ~~control flow meters~~

3rd seal leakage was measured by "dipping level" gauge located on RC DT panel behind racks.

Typical leakages were in gallons per hour. These were not accounted for in computer listed "identified" leakage^(IL) and would only present a problem if the computer printed IL exceeded the T & allowed 10 gpm.

~~Flow QPM = K x time~~

$$\text{Flow QPM} = K \times \text{display}$$

$$K_{1A} = 16.1$$

$$K_{1B} = 14.3$$

$$K_{2A} = 14.4$$

$$K_{2B} = 13.6$$

Talk to Jim Floyd

~~# Temperature~~

later Why like VS S

occurrences

Temperature \pm °F \approx repeatability

Pass Level \pm 1" \approx 2R 4" acc

RCD Voltage \pm Level 2 max 1

HOT Level \pm 1" acc

4.16 2 1% full range
gal punch in Central see CR

K-13

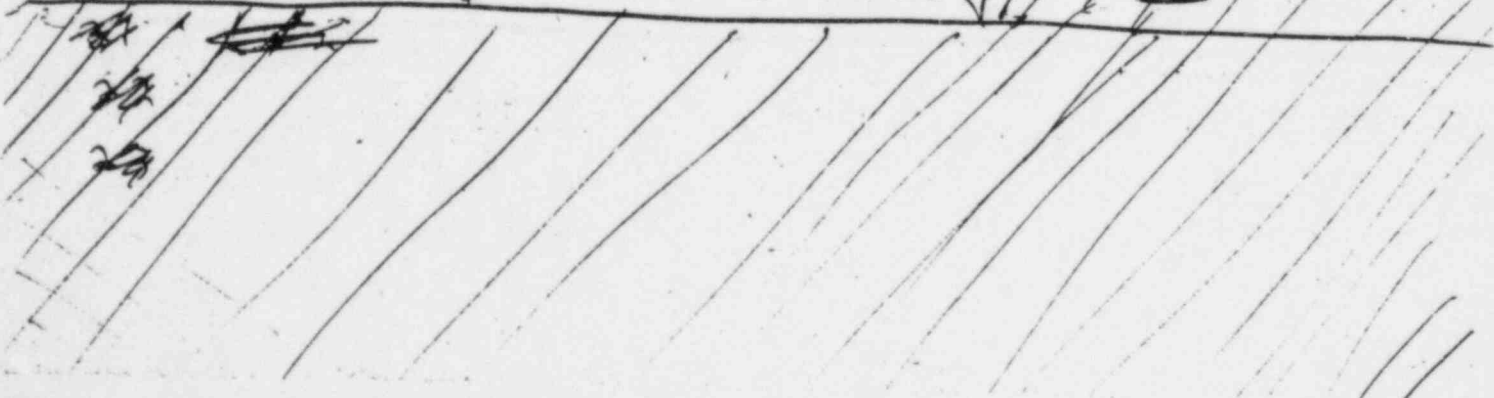
Hand Calculations
and Calculator notes

MEMORIES MAIN

TMI-2 constant

0 ~~Memories~~ $\Sigma \Delta M$

		data in	LD →
1	(21) (LM2)	(41) (ΣV_0 Terms)	
2	22 (L01)	42 $-1\frac{2}{3}$	
3	23 (L02)	43 6485	
4	24 066 HO MUT	44 P2 ΔM	
5	25 $P_i P \rightarrow T$	45 10678 1034	
6	26	46 V_{zi}	ΔM
7	27	47 M_{zi}	
8	28	48 25.7 $\frac{F_{wh}}{A}$	
9	29	49 1.34 $\frac{2886}{60}$ $\frac{62.0}{40}$	
10	30 2100 v_{ch}	50 $V_{0 \text{ cal}}$ $\frac{M}{D}$	
11	31 -5×10^{-7}	51 500268696 A	
12	32 ($T_i - 580$)	52 $\Sigma \Delta M$	
13	33 3.9×10^{-5}	53 GWR	
14	(T1) \downarrow	34 (ΣV_{ch} Terms)	54
15	(T2)	35 7×10^{-7}	55
16	(P1)	36 102240	56
17	(P2)	37 (Internal P_i) \downarrow	57
18	(Lz1)	38 M_7 $LD \rightarrow V_0$	58
19	(Lz2)	39 ($L_i - 77$)	59
20	(Lm1)	40 73.33333	



$$\begin{array}{ll}
 M = \text{mass (\#)} & L = \text{level (in)} \\
 \rho = \text{density (\#/ft}^3\text{)} & T = \text{Temperature (}^\circ\text{F)} \\
 V = \text{Vol (ft}^3\text{)} & \#/\text{Hr} \quad \psi = \frac{1}{\psi}
 \end{array}
 \quad (7)$$

$$\text{GLR} = \frac{(\Delta M_T + \Delta M_Z + \Delta M_M + \Delta M_C) \left(\frac{17.4805 \text{ gal}}{\text{ft}^3} \right)}{60 \text{ min/Hr}} \left(\frac{46.4 \text{ \#}}{\text{ft}^3} \right)$$

Temperature change

$$\Delta M_T = RC \psi \text{ Temp change} = (\rho_1 - \rho_2) 10678 \text{ ft}^3$$

Pressure change

$$\Delta M_Z = \rho_{z1} V_{z1} - \rho_{z2} V_{z2}$$

$$V_{z1} = 800 \text{ ft}^3 + (L_{z1} - 209) 3.208 \text{ ft}^3/\text{in}$$

Make Up Tank

$$\Delta M_M = (L_{M1} - L_{M2}) 255 \text{ \#/in}$$

~~ILR~~
Operator additions

$$\Delta M_C = (\text{gallons added}) 8.33 \text{ \#/gal}$$

$$\text{ILR} = \frac{(V_{2 \text{ gal}} - V_{0 \text{ gal}}) \frac{62.3009}{46.4}}{60}$$

main

Main Program
Table A

$$ULR = GLR - ILR$$

$$GLR = \frac{(\Delta M_1 + \Delta M_2 + \Delta M_M + \Delta M_o) \# \text{ Ngal} / \#}{60 \text{ min} / \text{Hr}}$$

$$N \text{ gal} / \# = \frac{1 / 46.4 \# / \text{ft}^3}{7.4805 \text{ gal} / \text{ft}^3} = .161218 \text{ gal} / \#$$

$$GLR = \frac{\sum \Delta M \cdot .161218}{60} = .00268696$$

$$ILR = \frac{(V_{RCDT_2} - V_{RCDT_1}) \frac{62.31}{46.4} \frac{1}{60}}{60}$$
$$= (V_{D2} - V_{D1}) (.022381)$$

$$V = \pi \left(4 - \frac{.347}{12}\right)^2 H = 49.541354 \text{ H ft}^3$$

Unidentified Leak Rate (ULR) =

Gross Leak Rate (GLR) - Identified Leak Rate ILR

$$GLR = \frac{\Delta M_{RC3} + \Delta M_{P22} + \Delta M_{MUT} + \Delta M_{OCF}}{\rho_{TAV12} (\cancel{62.4 \text{ lb/ft}^3}) (7.4805 \text{ gal/ft}^3)}$$

$$ILR = \frac{\Delta M_{RCRT} + \Delta M_{OCDT}}{\rho_{TAV12} (\cancel{62.4 \text{ lb/ft}^3}) (7.4805 \text{ gal/ft}^3)}$$

$$ULR = GLR - ILR$$

ΔM_{RCS} = Mass change due to RCS temperature change (lbs)

$$= \frac{V_{RCS1}}{\rho_{RCS1}} - \frac{V_{RCS2}}{\rho_{RCS2}}$$

Where: $V_{RCS} = 10,678 \text{ ft}^3 + (582^\circ\text{F} - T) \times 0.1 \text{ ft}^3/\text{F}$

ρ_{RCS} = ρT and is calculated by equation 18, p 21 from Keenan and Keyes - "Thermodynamic Properties of Steam"

ΔM_{PZR} = Mass change in pressurizer (lbs)

$$= \frac{V_{PZR1}}{\rho_{PZR1}} - \frac{V_{PZR2}}{\rho_{PZR2}}$$

$$V_{PZR} = 800 \text{ ft}^3 + (L - 200 \text{ in}) 3.208 \text{ ft}^3/\text{in}$$

ρ_{PZR} = ρT by equation 18 from K & K

$$\text{and } T = \rho P =$$

$$649.46 - (2200 - P_{PZR}) \cdot 0.0655 \\ - (2200 - P_{PZR})^2 (1.5 \times 10^{-5})$$

~~4500g~~

Use $\Delta M_H = (L_1 - L_2) 255 \text{ #/in}$ based on
 Tank dimensions
 and 3.6 #/cc ^{calib} procedure

$\Delta M_{MUT} = \text{Mass Change in Make up Tank (lb)}$

$$= \frac{V_{MUT1} - V_{MUT2}}{CV_{MUT1} - CV_{MUT2}}$$

not good because
 DP measurement
 is mass measurement

$V_{MUT} = 508 + (L - 65_{in}) 4.128446 \text{ ft}^3/\text{in}$

$CV_{MUT} = \text{FT by eq 18 from K \& K}$

$\Delta M_{OCP} = \text{Operator Changes to}$
 Primary (incl. MUT) (lbs)

$= (\text{Gallons in}) (7.48 \text{ gal/ft}^3) (2.4 \text{ #/ft}^3)$

$\Delta M_{RCOT} =$ Mass Change in RC Drain Tank

$$\Delta M_{RCOT} = \frac{V_{RCOT1}}{C_{V_{RCOT1}}} - \frac{V_{RCOT2}}{C_{V_{RCOT2}}}$$

$$V_{RCOT} = 6485 + 73.3353(L-77) - 1(L-77)^2$$

$C_{V_{RCOT}} = 9T$ by eq 18 from K & K

$\Delta M_{ocOT} =$ operator changes to RC Drain Tank

$\frac{55.0}{32.4}$
 2.21
 3068.87366
 3068.87366
 10266173971

Memories

- 0 582
- 1 10678
- 2 -0.1
- 3-13 ΔMRC scale
- 14 ΔMRC scale
- 15 4.6×10^{-7} } Comp Lig Curve, SBR
- 16 3.7×10^{-4} }
- 17 2200 psi
- 18 65
- 19 4.128446
- 20 508
- 21 6485
- 22 77
- 23 73.33333
- 24 -1.0
- 25-29 P \rightarrow T subroutine
- ~~28~~ ~~200~~
- ~~29~~ ~~3.208~~
- (30) ~~800~~ 17.46805
- 31 $V_{RCOT} (L-77)$
- 32 $V_{RCOT} \sum \text{terms} (6411 + 73.33(L-77) - (L-77)^2)$
- 33 ~~Tan~~ α
- 34 ΔV_{RCOT}
- 35 MRC_1
- 36 ~~MRC~~ MRC_2
- 37 ~~V~~ V_{PZ}
- 38 ~~MRC~~ V_{MUT}
- 39 ~~MRC~~

- ~~RCH 33~~
~~40~~
 41 200
 42 7.208 } Δ MP2R
 43 800 }
 44 P₁
 45 P₂
 46 MRC₁
 47 $\Sigma \Delta M$
 48 MP2R₁
 49 T_{an} 1
 50 T_{an} 2
 51 M_{HUT} 1
 52 ~~gal/#~~ #/gal at 72°F) = 83238 #/gal
 53 Gross I.R. gal/min
 54 (gal/# at T_{an})
 55 MRC_{DT} 1
 56 Δ MRC_{DT}
 57 I.R. gal/min

48
27
50

85

P-T	SBR	209-42	213
M	SBR	48-17	124-212
MRCOTi	SBR	87-17	84
MRCsi	SBR	70-81	
MP2Ri	SBR	240-	266
MHUT	SBR	270-	296
Main Program		301	

31
32
33
34
35 119 2
36 116 2
37
38
39 113
- 114

65
43

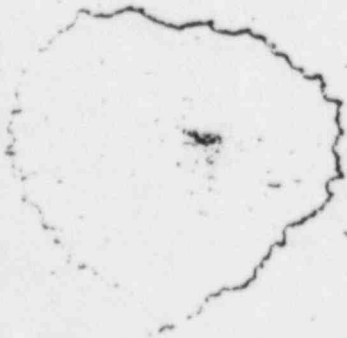


$$T_{PZR} = 5 P_{PZR} =$$

$$649.46 - (2200 - P_{PZR})(0.655) - (2200 - P_{PZR})^2 (1.5 \times 10^{-5})$$

$$\text{D} \quad V_{RCs} = 10,678 -$$

$$V_{RCs} = 10678 - (582 - T) \left(0.7 \frac{ft^3}{of} \right)$$



SBR ~~M~~ PZR 1

1 R/S Enter L PZR i
 2 ~~PRT~~
 34 RCL ~~41~~ (200)
 5 = (L - 200)
 6 X
 78 RCL ~~42~~ (3,208)
 8 = (L - 200)(3,208)
 90 +
 112 RCL ~~43~~ 800PTS
 13 = (VPZR = 800 + (L - 200)3,208)
 1415 ~~STO~~ 37

~~RCL 23
 +
 RCL 17
 (200 - PRES)~~

1178 SBR 213 ~~119~~ P → T Printer T needs P in 25
 19201 SBR 124 ~~118~~ W4 from T
 22 1/x PZR 1
 23 X
 24 25 RCL 37 VPZR 1
 26 = MPZR 1
 27 ~~STO~~ 2nd INU SBR

SBR ~~MRC~~ MRCs

1 20 R/S (Enter TCA₂)
 2 PRT
 3 +
 4 R/S (enter THA₂)
 5 PRT
 6 +
 7 R/S (enter TCB_i)
 8 PRT
 9 +
 10 R/S (enter THB_i)
 11 PRT
 12 =
 13 ÷
 14 4
 15 = (Tavg)
 16 17 STO 33 Tan
 18 PRT
 19 20 21 SBR ~~#8~~ 124 (n₄ SAT)
 22 23 STO 34

 24 ~~SBR (clear)~~
 25 26 SUM 34
 27 28 RCL 34 (n₄)
 29 PRT (n₅)
 30 31 RCL 33 (Tan)
 32 +/- (-Tan)
 33 +
 34 35 RCL 00 (582)
 36 X
 37 38 RCL 02 (-0.1)
 39 = -(582 - Tan)(0.1)
 over

Tent
 STO 2000 n₂₅
~~SBR 20~~
~~TAN 215~~
 enter 578
 579
 581
 582
 PRT 580
 RET n₄ CL

RCL 25 (P)
 -
 RCL 14 (2000)
 =
 X
 RCL 15 (4.6 x 10)
 =
 +
 RCL 16 (3.7 x 10)
 =
 +/-

40
4142 $\frac{+}{RCH\ 01}$ (10678)

43 = $\sqrt{RCS\ i} = (10678 - (582 - \text{Tax})(0.1))$

44 $\frac{\div}{RCH\ 34}$ $\sqrt{RCS\ i}$

47 = $MRCs\ i$

48 2nd INV. SBR

SBR MAUT_i

- 1 R/S (enter LMUT_i)
- 2 ~~---~~
- 34 RCL 18 (65)
- 5 = (LMUT_i - 65)
- 6 X
- 78 RCL 19 4.128446 ft/in
- 9 = (LMUT_i - 65) 4.128446
- 10 +
- 11-12 RCL 20 (508)
- 13 = VMUT_i = 508 + (L - 65) 4.128446
- 14-15 STO- 38 VMUT_i
- 16 R/S (enter TMUT_i)
- 17-19 SBR 124 ~~78~~ (VMUT_i)
- 20 V+ PMUT_i
- 21-23 XSRCL 38 VMUT_i
- 24 = MMUT_i
- 25 and INV SBR

SBR ~~118~~ MRCOTI 84

Dame

R/S enter LRCOTI

~~colca~~ VRCDTI in 32

R/S enter TRCDTI

PRT

SBR 118

~~VRCDTI~~

X

PRCDTI

RCL 32

VRCDTI

=

~~M~~ RCOTI

Incl INV SBR

Main Program

$$\begin{array}{r} 580.4 - 582 \\ 44.66 \quad 44.56 \end{array}$$

$$\begin{array}{r} 44.66 \quad 582.0 \\ 44.56 \quad 580.8 \\ \hline .10 \quad \underline{\underline{1.2}} \end{array}$$

$$44.66 + (T - 580.4) \left(\frac{-1}{1.2} \right) = \frac{44.66 - (T - 580.4)(0.833333)}{1.2} = 44.66 - (T - 580.8)(.0833333)$$

$$P_i = (10678 \text{ ft}^3) [44.66 - (T - 580.8)(.0833333)] \text{ #/ft}^3$$

$$\Delta M_{RCS} = (DNI - DNF) 10678$$

$$= 10678 \times \left\{ [44.66 - (T_1 - 580.8)(.0833333)] - [44.66 - (T_2 - 580.8)(.0833333)] \right\}$$

$$\Delta M_{PZR} = (L_{PZR1} - L_{PZR2}) 120.8$$

$$\Delta M_{MOT} = (L_{MOT1} - L_{MOT2}) 255.0$$

$$G-LR = (\Delta M_{RCS} + \Delta M_{PZR} + \Delta M_{MOT}) \left(\frac{T_1 + T_2}{2} \right) \text{ #gal/#}$$

$$\text{Gal/#} = \left[.16740 + (T - 580.4)(.0002923) \right] \frac{60}{580.4}$$

$$\begin{array}{r} 583.0 \quad .16816 \\ 580.4 \quad .16740 \\ \hline 2.6 \quad .00076 \\ \hline 2.6 \end{array}$$

07 P_T
~~08~~
~~09~~
~~10~~

Enter data

T₁ 01
 T₂ 02
 ✓ L_{Z1} 03
 L_{Z2} 04
 L_{MUT1} 05
 L_{AUT2} 06

10	.08333333
11	.0602923077
12	580.8
13	44.66
14	10628
15	120.8
16	255

Calc ΔMRCs ~~STO~~ 20

Calc ΔMZ ~~SUM~~ 20

Calc ΔMUT
 PRT ~~SUM~~ 20

Calc qpl/#

÷ GG = G Leak Rate
 PRT and STO

17	580.4 580.4
18	.16740
19	
20	
21	ΔMRCs

2nd LBL A

for GHR Calc R/S Enter Date
enter T₁ PRT
ADV

R/S

STO 01

PRT

R/S

enter T₂

STO 02

PRT

R/S

enter L₂₁

STO 03

PRT

R/S

enter L₂₂

STO 04

PRT

R/S

enter L_{MUT1}

STO 05

PRT

R/S

enter L_{MUT2}

STO 06

PRT

RCL 01

T₁

-

RCL 12

580.8

=

T₁ - 580.8

X

RCL 10

.08333

=

(T₁ - 580.8) .08333 —

+/-

- "

+
 RCL ~~13~~ 13 44.66
 = P_{T_1}
 STO 07 P_{T_1}
 RCL 02 T_2
 -
 RCL 12 580.8
 = $T_2 - 580.8$
 X
 RCL 10 .0833
 = $(T_2 - 580.8) \cdot 0833$
 +/- - 11

+
 RCL ~~13~~ 13 44.66
 = P_{T_2}
 +/- - P_{T_2}

+
 RCL 07 P_{T_2}
 = $P_{T_1} - P_{T_2}$

X
 RCL 14 10678 ~~10678~~ Vol Res
 = $\Delta MRCs$

~~STO 20~~ $\Delta MRCs$ \leftarrow register
~~PRT~~

RCL 03 L21
 -

RCL 04 L22

= $L_{21} - L_{22}$
 X
~~120.8~~ RCL 15 120.8 #/in (P20)
 = ΔM_{PLR}
~~SFO~~
 SUM 20 $\Sigma \Delta M$
 PRT
 RCL 05 L_{MUT1}
 -
 RCL 06 L_{MUT2}
 = $L_{MUT1} - L_{MUT2}$
 X
 RCL 16 255 #/in (MUT)
 = ΔM_{MUT}
 SUM 20 $\Sigma \Delta M = \Delta M_{RCS}$
 PRT
 RCL 01 T_1
 +
 RCL 02 T_2
 = $T_1 + T_2$
 ÷
 2
 = $(T_1 + T_2) / 2 = T_{AV}$
~~SFO 08~~
~~RCL 08 T_1~~
 -
 RCL 17 580.4

$$= T_{av} - 580.4$$

X

$$RCH \quad 11 \quad .0002923 \quad -$$

=

$$(T_1 - 580.4) \cdot 0002923$$

+

$$RCH \quad 18 \quad .16740$$

=

gal/#

PRT

gal/#

X

$$RCH \quad 20 \quad \Sigma \Delta M$$

=

~~11111~~ Total gross leakage

÷

60

0

=

$$GLR - gpm$$

Enter P Start

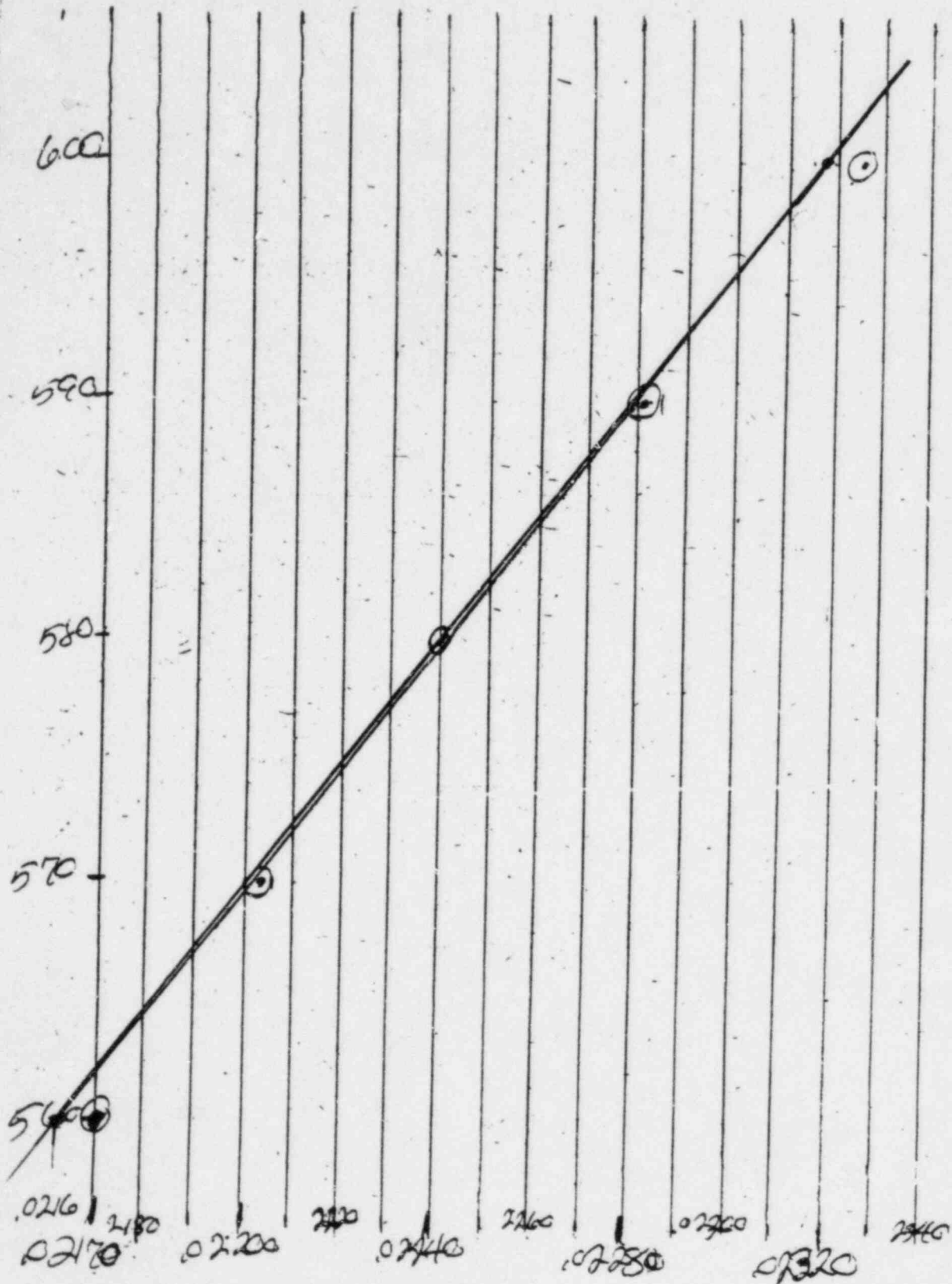
STC 25

~~R/S Enter T~~

SBR 20

Enter T R/S 4 times

~~R/S~~ Return



mod 2 BL A

R/S enter Date i

STO 00

R/S enter Time

STO 01

R/S enter hi

STO 02

R/S enter ~~OT~~ P_i

STO 03

R/S enter ~~TT~~ P_i

STO 04

~~R/S~~ enter Date i + 1

STO 05

R/S enter Time i + 1

STO 06

R/S enter hi + 1

STO 07

R/S ~~enter~~ OT P_{i+1}

STO 08

R/S enter TT P_{i+1}

STO 09

RCL 00 Date i

PRT Date i

~~RCL~~ 05 Date i + 1

059 STO 00 Date i

RCH 07 k_{i+1}

RCH 02 k_i

PRT ΔL

STO 10 ΔL

RCH 08 OTP_{i+1}

71

RCH 04 TTP_i

PRT P_j

STO 11 P_i

RCH 10 P_i

X ΔL tt

~~RCH 20~~ 209.45456 gal/ft

+

~~RCH 11~~ P_i

~~X~~

~~RCH 21~~ 244.3636533

90

STO 12

RCH 06

÷

1

0

0

Gross UID Leakage
 T_{i+1}

=
 2nd Int
 STO 13 Int of T_{i+1}
~~STO 13~~ T_{i+1}
~~STO 13~~
~~STO 13~~
~~STO 13~~
 ÷
 1
 00
 =
 =
 =
 RCH 13 Int T_{i+1}
 =
 X
~~100~~ 1
~~100~~
~~100~~
 +
 6
 0
 X
 RCH 13
 +
 2
 4
 X
 6
 0
 =

STO 14
RCL 01 T_i

÷
1
0
0
=

mod Int

STO 13 Int of T_i
RCL 01 T_i

÷
1
0
0
-

RCL B
=

X

1
0
0

+

60

X

RCL B

=

÷-

+ RCL 14 Ti+1 min
= ΔTi

~~1/4~~
X

RCL 12 GUL

=

PRT

~~B~~ UK GPM

RCL 06 Ti+1

~~STO~~ 01 Ti

RCL 07 Li+1

STO 02 Li

RCL 08 OTPi+1

STO 03 OTPi

RCL 09 TTPi+1

STO 04 TTPi

~~ADV~~ 2ND ADV

2nd ADV

GTC ~~B~~

Normal Value	Parameter	Unit	Range	Installation	Instrument	Relief Ventilation	No. of Measurements	Ventilation in Average	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium
580	Hot leg A temp 1	THA1	520 - 620	± 2"	± 2"	± 2"	3	± .163	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium
(Over of all)	Hot leg B temp 1	THB1	520 - 620	± 2"	± 2"	± 2"	3	± .163	(4) 46.4 #/ft ³ (60 #/ft ³)						
T.A.	Cold leg A temp 1	TEA1	520 - 620	± 2"	± 2"	± 2"	3	± .163							
580	Cold leg B temp 1	TEB1	520 - 620	± 2"	± 2"	± 2"	3	± .163	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium
(Over of all)	Hot leg A temp 2	THA2	520 - 620	± 2"	± 2"	± 2"	3	± .163	(0.346) (0.176 #/ft ³) (7.185 #/ft ³)						
T.A.	Hot leg B temp 2	THB2	520 - 620	± 2"	± 2"	± 2"	3	± .163	(46.4 #/ft ³) (60 #/ft ³)						
2155	Cold leg A temp 2	TEA2	520 - 620	± 2"	± 2"	± 2"	3	± .163	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium
2155	Cold leg B temp 2	TEB2	520 - 620	± 2"	± 2"	± 2"	3	± .163	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium
200	RC Steam	P1	1700 - 2500	± 20 PSI	± 20 PSI	± 20 PSI	1	± 20	(4) 60 #/ft ³						
200	RC Steam	P2	1700 - 2500	± 20 PSI	± 20 PSI	± 20 PSI	1	± 20	(10.346) (0.176 #/ft ³) (10.346) (0.176 #/ft ³)						
70	RC Level 1	LZ1	0 - 400	± 1"	± 1"	± 1"	3	± 1.55	(500) (0.0193 #/ft ³) (16.2 #/ft ³)						
70	RC Level 2	LZ2	0 - 400	± 1"	± 1"	± 1"	3	± 1.55	(10.346) (0.176 #/ft ³) (10.346) (0.176 #/ft ³)						
70	MUT Level 1	LM1	0 - 100	± 1"	± 1"	± 1"	3	± 1.04	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium
70	MUT Level 2	LM2	0 - 100	± 1"	± 1"	± 1"	3	± 1.04	(57.4 #/ft ³) (7.185 #/ft ³) (46.4 #/ft ³) (60 #/ft ³)						
77	RCDT Level 1	LD1	0 - 92	± 1"	± 1"	± 1"	3	± 0.58	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium
77	RCDT Level 2	LD2	0 - 92	± 1"	± 1"	± 1"	3	± 0.58	(62.3 #/ft ³) (7.185 #/ft ³) (46.4 #/ft ³) (60 #/ft ³)						
58100	Operator Changes	Mo	No Limit	± 1 gal	± 1 gal	± 5 gal	1	± 5	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium	Partial Equilibrium

R115

>

112.8

1.8756

1.837

1.98

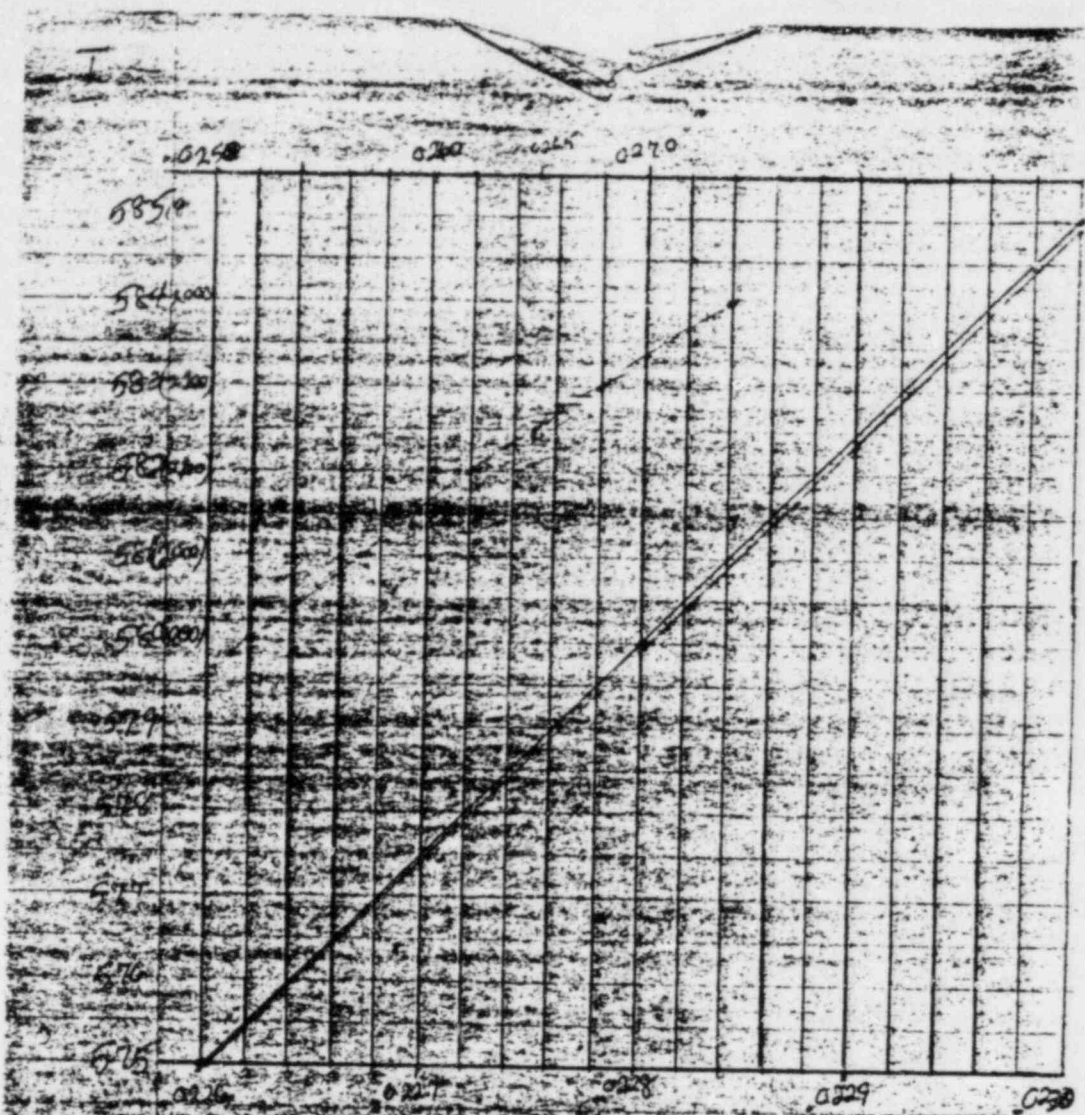


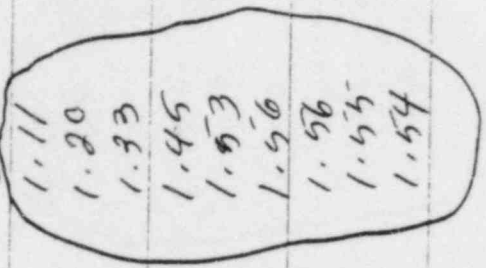
Table 1 (44.478 - 43.478) / 10.5 = 0.09452674 #/F
 Table 2 (44.228 - 43.478) / 10.5 = 0.07173
 = 0.0775 #/ft #/F

General R = MAT I H O P E R T P I D H V T

= $\frac{1}{2} (T_1 - T_2) \cdot 0.0775 \text{ #/ft}^3 / \text{F} \cdot (10,678) \text{ ft}^2$
 + $\frac{1}{2} (L_1 - L_2) \cdot 3008 \text{ ft}^2 \cdot 37.70739 \text{ #/ft}^3$
 + $(L_{HT} - L_{HT}) \cdot 255 \text{ #/in} \cdot \frac{1}{62.42197} \cdot 7.4805$

Date Unidentified Leakage Date Unidentified Leakage Date Unidentified Leakage

4/18	0.85	2/16	0.05	3/11	0.55
5	0.48	17	0.08	12	0.13
6	0.48	18	0.12	13	0.43
7	0.74	19	0.25	14	0.48
8	1.18 (1.12)	20	0.36	15	0.64
9	1.40	21	0.50	16	0.85
10	1.72	22	0.57	17	0.91
11	2.07	23	0.62	18	1.11
2/12	2.27	24	0.70	19	1.20
2/2		25	0.73	20	1.33
3		26	0.76	21	1.45
4		27	0.75	22	1.53
5		28	0.75	23	1.56
6		3/1	0.73	24	1.56
7		2	0.77	25	1.55
8		3	0.77	26	1.54
9		4	1.04	27	
10		5	1.10	28	
11		6	0.95		
12		7	1.04		
13	0.0	8	1.10		
14	0.0	9	0.99		
15	0.0	10	0.78		



WET A' ~~Write Data Entry Routine~~ 16-63 14-23
 Store ^{Date} ~~(L1, T2)~~ (P1, P2) L21, L22 L41, L42 L01, L02 cc

ET ~~Cable~~ Cable routine 121-201 3-13

ET D Cable P-T routine 202-280 25-29
 P1 stored in T2, T2 out

WET B' Write Vcc routine 453 steps 8 BFO1
 T2 in P1 stored in 37, Vcc out 45-108

WET B Write ΔM1 routine 265-295 2 Mem
 Data stored data, ΔM1 out

WET C Write ΔM2 routine 320-368 2 Mem
 Data stored data, ΔM2 out

WET D Write ΔM3 routine (Use L1-L2) Const
 Data stored input data, ΔM3 out 370-384

WET E Write ΔM4 routine (Use V1-V2) Const
 Will ^{store} input data, ID lead out 385-406

WET A Write Menu routine 410-
 Entered by Pressing A. Enter Date Per A'

Print	10 data entries	10
V1, V2	V1, V2, V1, V2	2
ΔM1, ΔM2, ΔM3, ΔM4		4

WET C Write L2in → V2out 300-319

WET E' AD level → V0 routine 3 steps 6 Mem
~~L01~~ L01 in V0 out 233-242

11 12 13 14 15 16 17 18 19 20
 A B C D E A' B' C' D' E'

Date Time

A' 1463 -
 B' 65-108
 C' 111-201
 D' 202-230
 E' 233-262
 B 265-295
 C 300-368 (SARCE) 300-319
 D 370-384
 E 385-406
 A 480-459

Data T₁ T₂ P₁ P₂ L_{z1} L_{z2} L_y L_x L_D L_{D2}
 View OCCup
 vs
 P → T
 L_D - V_D
 ΔMT
 ΔM₁
 ΔM₂
 Main

Prints

spoc → all data #
 Date, Time 11 parameters

sp →
 Answers
 sp
 mass Total
 sp
 QLR
 ILR
 ULR

2nd LBL A

SRBMA'S

Enter Data Printer

~~2nd LBL A~~

SRB ΔM_T Printed

STO 52 ΔM_T

SRBC ΔM_Z Printed

SUM 52 ΔM_T + ΔM_Z

SRBD ΔM_M Printed

SUM 52 ΔM_T + ΔM_Z + ΔM_M

RCH 24 OCC Water entered by operator

X

8

0

3

3

~~PRT~~ ΔM₀

SUM 52 Σ ΔM_{RCS}

~~RCH~~ RCH 52 Σ ΔM_{RCS}

~~PRT~~ ADV

PRT Σ ΔM_{RCS}

X RCH 51 G.H.R. conversion to GPM. 00268644

~~STO~~ STO 53 G.H.R.

PRT G.H.R.

SRBE I.H.R. Printed

+/-

~~RCH 53~~ +

RCH 53

$$\frac{1}{46.4 \frac{1}{100}} \times 7.485 \frac{1}{100}$$
 GC

1040 ~~LRM~~ LRM

Data entry

①

- 2 Label A'
- 3 Advance Times
- 5 Enter Date
- 6 Print
- 7 advance

47	Enter	T12	P12	L212	L412	L012
	Print	14-15	16-17	18-19	20-21	22-23

48 ~~Advance~~

49 ~~NO SBR~~

= U.L.R.
PRT
ADV
ADV
GTOA

~~Head~~ KCH $\frac{1}{16}$
 STO ~~37~~
 RCH ~~38~~
 SBR B'

Pi in SBR C' 1000 (2)
 Ti

43 steps & Storage
~~Table~~ Curve fit to ASME Tables

2 2nd LBL B'

~~3~~
~~4~~
~~5~~ ~~38~~ (C'1) ~~1000~~
 =

8 STO 32 (C'2) (Ti - 580)

X
 11 RCL 33 (C'3) (3.9 x 10⁻⁵)
 =

14 STO 34 (C'4) (3.9 x 10⁻⁵ (Ti - 580)), $\Sigma \sqrt{\text{Terms}}$
 15 ~~REL~~ 32 (C'2) (Ti - 580)

17 X²
 18 X

20 RCL 35 (C'5) (2.00 x 10⁻⁷)
 21 =
 22 (Ti - 580)² (2.00 x 10⁻⁷)

23 SUM 34 ($\Sigma \sqrt{\text{Terms}}$)

25 RCL 36 (C'6) (1.02240)

26 SUM 34 $\Sigma \sqrt{\text{Terms}}$

29 RCL 37 (C'7) Internal Pi

31 ~~31~~
 32 RCL 30 (C'8) 2100
 33 =
 34 (Pi - 2100)

35 X
 36 RCL 31 (C'9) (5 x 10⁻⁷)
 37 =

39 SUM 34 (C'4) $\Sigma \sqrt{\text{Terms}}$

40 RCL 34
~~41~~
~~42~~
 INV SBR

For error analysis
 PZR fluctuating 60-80 PSI
 Mike Benson

$$P_{\text{corr}} = .00005 \text{ ~~AAAAA~~}$$

$$P_{\text{err corr}} = \frac{.00005(P-2100)}{100} = \frac{5 \times 10^{-7}(P-2100)}{100}$$

$$\text{~~0.02240~~} + (T-580) \frac{3.9 \times 10^{-5} \cdot 0.0256}{40} + (T-580)^2 2.25 \times 10^{-7}$$

$$\sigma_y = .02240 + (3.9 \times 10^{-5})(T-580) + 2.25 \times 10^{-7}(T-580)^2$$
~~$$+ (-5 \times 10^{-7})(P-2100)$$~~

$$.02317 \quad (T-580)^2 t = .00009$$

$$.02161$$

$$\frac{.00156}{40} \quad t = \frac{.00008}{400} = \frac{8}{4} \times 10^{-7} = 2.0 \times 10^{-7}$$

$4 \sqrt{.00156}$
 39
 12
 76

128
 64

+ 256

$\frac{2.5}{4}$
 $\frac{2.5}{4}$
 $\frac{2.5}{4}$

2×10^{-7}

600 02377
 02326
 0051

590 0230625
 02281
 002525

570 02203
 0217825
 0002475

02170
 2121
 49

	2000	2100	2200
600	02332	02320	02320
590	02286	02281	02275
580	02245	02240	02235
570	02207	02203	02199
560	02173	02170	02166

Needs Ld
and hbl and E

$Ld \rightarrow Vb$

(5)

~~RA RCH~~

~~RE~~

30 steps
6 minutes

34
are
previous
programs

~~of R/S under~~
~~part~~

- 5 -
- 6 RCH 38 77
- 8 = (hi? - 77)
- 10 STC 39 (hi - 77)
- 11 X
- 12 RCH 40 73.33333
- 13 = (hi - 77) (43.33333)
- 14 = " Σ terms
- 15 STC 41
- 16 RCL ~~39~~ (hi - 77)
- 17 X²
- 18 X
- 19 RCH 42 (-1)
- 20 = - (hi - 77)²
- 21 SUM ~~41~~ Σ terms
- 22 RCH 43 6485
- 23 SUM ~~41~~ (24 - 77) 73.33333 + (hi - 77) (-1)
- 24 ~~RCH 41~~ + 6485
- 25 INU SBR

35 steps 2

7

U is many

$$\Delta M_T = 10678(P_1 - P_2)$$

1	2nd L B 2 B	
2	RCL 17	(P ₂)
3		(C 7)
4	STO 37	(T ₂)
5	RCL 15	(P ₂)
6	SBR B'	(B ₁) P ₂
7	STO 44	(P ₁)
8	RCL 16	(C 7)
9	STO 37	(T ₁)
10	RCL 14	(P ₂)
11	SBR B'	
12		
13		
14	RCL 44	B ₁ - P ₂
15	=	P ₁ - P ₂
16	STO X	STO
17	RCL 45	= P ₂ 10678
18	=	$\Delta M_{RCS} = \Delta M_T$
19	STO	STO
20	STO	STO
21	STO	STO
22	STO	STO
23	PRT	
24	INV SBR	

$\Delta M_z = V_{z2} P_{z1} - V_{z1} P_{z2}$

$V_{zi} = 800 + (h_i - 200) 3.208$ (SBR CE)

$P_{zi} = \frac{M_{zi}}{V_{zi}}$

2nd hBh C

RCL 19

SBR CE

STO 46

RCH 17

STO 25

SBR and D'

SBR and C'

$\frac{1}{h}$

X

RCL 46

=

STO 47

RCH 18

SBR CE

STO 46

RCH 16

STO 25

SBR and D'

SBR and C'

$\frac{1}{h}$

X

RCL 46

=

h_{z2}

V_{z2}

V_{z2}

P_{z2}

Internal P_i

T_{z2}

V_{z2}

P_{z2}

V_{z2}

$V_{z2} P_{z2}$

$V_{z2} P_{z2} = M_{z2}$

h_{z1}

V_{z1}

V_{z1}

P_{z1}

T_{z1}

V_{z1}

P_{z1}

V_{z1}

$V_{z1} P_{z1} = M_{z1}$

V_{z2}

STO

calc P_{z2}

X

V_{z2}

STO

ttt

—
RCL 47
=
PRT
IMV SBR

M₂₂
ΔM_z

8a

$I_{zi} \rightarrow V_{zi}$
Fund 2BL CE

~~0000~~ 2
0
0

=
X

3

0000

8

+

8

00

0

=

14

INU 9BR

$$\Delta M_m = (L_{M1} - L_{M2}) 255$$

(9)

2nd LBL D

RCH 20

L_{M1}

RCH 21

L_{M2}

=

$L_{M1} - L_{M2}$

X

RCH ~~20~~ 48

255 #/in

=

ΔM_m

PRT

INV SBR

① I.D. leak rate ILR ^{62.31}

~~ILR~~ $ILR = (V_2 - V_1) \frac{62.31}{46.4} \times 100$

$ILR = (V_2 - V_1) \frac{62.31}{46.4} = 1.342886/100$

2nd LABEL

RCL 22 LDR

SBR 2nd E' VDR

STO 50

RCL 23 LDR

SBR 2nd E' VDR

RCL 50 VDR

= ΔV_{leak}

X

RCL 49 $\frac{62.31}{46.4} = 1.342886/100 = .022381$

=

PRT

INV SAR

$$V_1 = 6485 + (1.1 - 1.0) 73.333 - (1.1 - 1.0)^2$$

~~W.A. H. C. H. D.~~

~~W.A. H. C. H. D.~~ $(V_2 - V_1) P_{min} 62.31 \# / ft^2 \cdot 1612 \text{ gal} / ft^2$

more compared to small compared to then $(1.0 - 1.1) 73.333 + (1.0 - 1.1)^2$ $\frac{293}{0}$ $\frac{10}{10}$ $\frac{10}{10}$ at rounded for "

$$P_{10} = 2 U_{10} \frac{1}{100} (62.31 \# / ft^2) = 2 U_{10} \frac{1}{100} 6485 + (1.1 - 1.0) 73.333 - (1.1 - 1.0)^2$$

$$= \frac{2 U_{10}}{100} P_{10} (1.0 - 1.0) 73.333 = \frac{2 U_{10}}{100} 62.31 \# / ft^2 \cdot 1612 \text{ gal} / ft^2$$

$$P_{10} = P_{10} (62.31 \# / ft^2) \frac{1}{100} (73.333 \# / ft^2) (1612 \text{ gal} / ft^2)$$

$$P_{10} = 20 \cdot 8.3454$$

$$P_{10} = 20 \cdot 8.3454 \frac{1}{100} (1612 \text{ gal} / ft^2)$$

W.A. H. C. H. D.

3
93

$$P_{R_2} = (2.51 \text{ #/ft}) (7.4805 \text{ gal/ft}^3)$$

$$P_{R_2} = (46.4 \text{ #/ft}^3) (60 \text{ Min/ft}^3)$$

254.4950
840
5000

$$\Delta P = 10346 \left(\frac{1}{V_{CL}} \cdot \frac{1}{V_{CL}} \right)$$

$$\Delta R_T = \frac{1}{.000} \frac{.02240 + (T - 580) 3.9 \times 10^{-5} (T - 580) \text{ (air)}}{2100} = \frac{.02240 + (T - 580) 3.9 \times 10^{-5} (T - 580) \text{ (air)}}{2100}$$

600	2100	2150	2200
42.992	43.048	43.103	
43.840	43.898	43.956	.111
44.643	44.693	44.743	.116
45.393	45.434	45.475	.100
46.083	46.126	46.168	.82
			.85

600	43.75	44.642817
590		44.565265
580		.077592
570		
560		

$$3.10 = .0776 \text{ #/ft}^3$$

$$R_T = \frac{R_{T_{air}} 0.0776 \text{ #/ft}^3 1.4805 \text{ gal/ft}^3}{(46.4 \text{ #/ft}^3) (60 \text{ Min/ft}^3)}$$

Computer errors %
By order of significance

③

also 7
end side

1. Failure to convert R.C.P. Volume change to
Reactor Temperature Conditions

2. Failure to convert water additions to MPT
to reactor temperature conditions

3. Truncation of Primary average temperature
above 582°F to 580°F

4. Failure to account for variations in Pressurizer
pressure.

5. Incorrect primary system volume

6. Incorrect ~~value~~ for density of Primary water
used for used in definition of gallons

7. Incorrect dMPT used for MPT mass change

8. Reactor Coolant Drain Tank Level

Unidentified leakage = Gross Leakage - Identified Leakage

$$\Delta M_T = \Delta M_T + \Delta M_{R,R} + \Delta M_{N,T}$$

$$\text{Identified leakage} = \frac{P_1(V_2 - V_1)}{P_2(V_2 - V_1)} (V_2 - V_1)$$

$$\Delta M_T = 10346(P_1 - P_2) = P_1 = \text{compressed liquid}$$

$$\Delta M_{1,2R} = V_1 P_1 - V_2 P_2 = \left[\frac{800}{2} + 200(h_1 - 200) \right] (P_1) - \left[\frac{800}{2} + 200(h_2 - 200) \right] (P_2)$$

$$\Delta M_{N,T} = 259(L_{M_1} - L_{M_2})$$

GARRA

$$U_{LR} = G_{LR} - I_{LR}$$

$$V_{2i} = \frac{3.19754 - 0.3151548(374.11 - t_2)^{1.5} - 1.203374 \times 10^{-2}(374.11 - t_2) + 7.48908 \times 10^{-13}(374.11 - t_2)^4}{1 + 0.1742489(374.11 - t_2)^5 - 3.946263 \times 10^{-3}(374.11 - t_2)^3}$$

$$x = \frac{649.46 - (2200 - P_2)(0.0655) - (2200 - P_2)^2(1.5 \times 10^{-5})}{9} - 32$$

$$V_{CLi} = .08240 + (T_i - 580) 3.9 \times 10^{-5} + (T_i - 580)^2 (2 \times 10^{-7}) - (P_i - 2100) (5 \times 10^{-7})$$

conversion to English units
 $(K) = 1.01602$

Identified leakage

Gross Leakage - Identified Leakage

$$\Delta M_T + \Delta M_{R,R} + \Delta M_{N,T}$$

$$\text{Identified leakage} = \frac{P_1(V_2 - V_1)}{P_2(V_2 - V_1)} (V_2 - V_1)$$

$$\Delta M_T = 10346(P_1 - P_2) = P_1 = \text{compressed liquid}$$

$$\Delta M_{1,2R} = V_1 P_1 - V_2 P_2 = \left[\frac{800}{2} + 200(h_1 - 200) \right] (P_1) - \left[\frac{800}{2} + 200(h_2 - 200) \right] (P_2)$$

$$\Delta M_{N,T} = 259(L_{M_1} - L_{M_2})$$

GARRA

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$$x = \frac{649.46 - (2200 - P_2)(0.0655) - (2200 - P_2)^2(1.5 \times 10^{-5})}{9} - 32$$

$$V_{CLi} = .08240 + (T_i - 580) 3.9 \times 10^{-5} + (T_i - 580)^2 (2 \times 10^{-7}) - (P_i - 2100) (5 \times 10^{-7})$$

$$dM_2 = V_{k1} P_2 - V_{k2} P_2 = (800 + (L_1 - 200) 3.208) P_2 - (800 + (L_2 - 200) 3.208) P_2$$

assume P_2 const since P_{atm} is handled separately.

$$dM_2 = 800 P_2 + L_1 (3.208) P_2 - (200) 3.208 P_2 - 800 P_2 - L_2 (3.208) P_2 + (200) 3.208 P_2$$

$$= (L_1 - L_2) 3.208 P_2 = P_{k2} \cdot 3.208 \frac{\text{ft}}{\text{min}} (L_2 + 215.5 \text{ ft}) = P_{k2} \cdot \frac{\text{in}}{\text{min}} (3.208 \text{ ft}^2) \cdot 39.69 \frac{\text{ft}}{\text{ft}}$$

$$dR_2 = dM_2 \frac{1}{60} \frac{\text{min}}{\text{hr}} = 11.4805 \frac{\text{gal}}{\text{ft}^3} \cdot 46.4 \frac{\text{ft}^3}{\text{hr}} = R_2 (3.208 \frac{\text{ft}}{\text{min}}) (39.69 \frac{\text{ft}}{\text{ft}}) (60 \frac{\text{min}}{\text{hr}})$$

$$\frac{P_2}{P_0} = \left(\frac{P_{M2}}{P_0} + \frac{L_1 P_2}{P_0} \right) \frac{1612 \text{ gal/ft}^3}{60 \frac{\text{min}}{\text{hr}}} = 44.643 \frac{\text{ft}}{\text{hr}}$$

$$= 44.743 \frac{\text{in}}{\text{hr}}$$

~~$$\frac{dR_2}{P_0} = \frac{dM_2}{P_0} = \frac{11.4805 \text{ gal/ft}^3 \cdot 46.4 \text{ ft}^3/\text{hr}}{60 \text{ min/hr}} = \frac{88.27 \text{ gal/ft}^3}{\text{hr}}$$~~

$$= \frac{1}{V_{c4}} - \frac{1}{V_{c1}}$$

~~$$P_{\text{atm}} (P_{\text{atm}}) = (10346 \text{ ft}^3) (0.001 \text{ #/ft}^3) P_{\text{atm}} (1612 \text{ gal/ft}^3) (60 \frac{\text{min}}{\text{hr}})$$~~

$$+ (800 \text{ gal}) (0.0793 \text{ #/ft}^3) P_2 (0.1612 \text{ gal/ft}^3) (60 \frac{\text{min}}{\text{hr}}) \cdot P_2 = P_{k2} [(10346 \text{ ft}^3) (0.001 \text{ #/ft}^3) + (800 \text{ gal}) (0.0793)]$$

$$P_2 = P_{k2} [(10346 \text{ ft}^3) (0.001 \text{ #/ft}^3) + (800 \text{ gal}) (0.0793 \text{ #/ft}^3)] (0.1612 \text{ gal/ft}^3) (60 \frac{\text{min}}{\text{hr}})$$

$\frac{dM_2}{P_0} = \frac{dR_2}{P_0}$

$$P_{k2} = 38.189$$

$$P_{200} = 37.396$$

$$\frac{dR_2}{dP} = \frac{1}{100} \frac{\text{ft}}{\text{hr}}$$

$$dM_2 = L_2 P_2 - V_{k2} P_2 = (800 + (L_1 - 200) 3.208) P_2 - (800 + (L_2 - 200) 3.208) P_2 = 800 \frac{dP_2}{dP}$$

K-14

Brief Notes on discussion with B. Smith

Interview
with
Bernie Smits

Hautman CRO Smith's shift K-14
Inventory Test

Have checked all files have
never exceeded 1 gpm every
three days.

Looking 1 gpm 50K days.
parameters changing
if came out > 1 gpm
would re-run.

Yes did sample up computer
results
Temp could attention to 4.03

Interferes that you have 72
hours to find find acceptable
leak rate

Temp c
Press c change in turbine
change with 100 gal water
could get 45 gal leak rate
guy could make up wasn't real.

Adding H₂ normal evolution
would change
compresses water in M.O.T.

In order to W. R.C.D.T level
calibration must ~~and~~ manually
input R.C.D.T level

Bernie
Hautman always felt he was under pressure