

International Agreement Report

Assessment of RELAP5/MOD2 Using LOCE Large Break Loss-of-Coolant Experiment L2–5

Prepared by Lainsu Kao, Kuo-Shing Liang, Jeng-Lang Chiou, Lih-Yih Liao, Song-Feng Wang, Yi-Bin Chen

Institute of Nuclear Energy Research P.O. Box 3, Lung-Tan 32500 Taiwan, Republic of China

Office of Nuclear Regulatory Research U.S. Nuclear Regulatory Commission Washington, DC 20555

April 1992

Prepared as part of The Agreement on Research Participation and Technical Exchange under the International Thermal-Hydraulic Code Assessment and Application Program (ICAP)

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ABSTRACT

Comprehensive analysis with RELAP5/MOD2 is performed to predict the LOFT transient thermal-hydraulic responses for the LOCE L2-5 test. Experiment L2-5 is planned to simulate a hypothetical LOCA which results from a 200% double-ended offset shear break in a cold-leg of a typical pressurized water reactor. The test simulation begins with break initiation and subsequent blowdown, and continues through lower plenum refill, core reflood, and terminates with corewide guench. The nominal best estimate calculation results indicate that the cladding temperature continuously increases during blowdown phase without an early fuel-rod rewet (blowdown guench). A peak cladding temperature of 1,112 K, which is very close to the experimental data, is calculated at 7.0 s, and fuel rods are predicted to be quenched at 57 s after the break initiation. Sensitivity analyses of the test simulation with respect to various code input uncertainties, including broken loop initial temperature, cross-flow junction, discharge coefficient, accumulator condition, reflood fine mesh number, form loss coefficient, fuel gap dimension, and reflood option are performed to investigate their impacts on the calculation results. Scenario study on the pump behavior is analyzed to see whether the blowdown quench could be resulted from the RELAP5/MOD2 model. The effect of the uncertainty of Biasi CHF on the cladding temperature response is also studied.

SUMMARY

This report documents the results and conclusions of the RELAP5/MOD2 code assessment in the analysis of LOCE test L2-5. Sensitivity studies of the L2-5 simulation with respect to various modeling options are performed as well to investigate their impacts on the calculation results.

LOCE L2-5 is performed to simulate a hypothetical LOCA which results from a 200% double-ended offset shear break in the coldleg of a typical pressurized water reactor. A specific purpose of L2-5 test is to establish conditions which will result in a large break blowdown without early quench that occurred during previous large break LOCA tests. RELAP5/MOD2 is an advanced, onedimensional, two fluid, six-equation, thermal nonequilibrium reactor transient and accident analysis program. The objective of this assessment study is to provide systematic assessment of the RELAP5/MOD2 code relative to code development, code improvement, and the enhancement of user guidelines.

In this study, the test simulations using RELAP5/MOD2 begin with break initiation and subsequent blowdown, and continue through lower plenum refill, core reflood, and terminate with corewide quench. Major events and their timings of the large break LOCA test L2-5 are well predicted by the RELAP5/MOD2 model. According to the hydraulic process (pump behavior) set up in L2-5, the RELAP5/MOD2 calculation gives no early quench phenomenon. Important parameters, such as pressure, break flow, and cladding temperature, are calculated with reasonable agreement in the comparison to the test data. Noticed differences between the calculation results and the test data including hot-leg break flow at initial period, cladding temperature during reflood, pressurizer pressure response, cladding temperature responses at upper and 1 wer elevations of the fuel rod, fuel quench temperature etc., are discussed with possible reasons in this report. On the other hand, the calculated peak cladding temperature (the most stated parameter concerned in a large break LOCA) of 1,112 K is in excellent agreement with the test data of 1,077 K.

Sensitivity analyses of the test simulation with respect to various code input uncertainties, including broken loop initial temperature, cross-flow junction, discharge coefficent, accumulator condition, reflood fine mesh number, form loss coefficient, fuel gap dimension, and reflood option are performed to investigate their impacts on the calculation results. Scenario study on the pump behavior is analyzed to see whether the blowdown quench could be resulted from the RELAP5/MOD2 model. The effect of the uncertainty of Biasi CHF on the cladding temperature response is also studied.

Calculated PCTs are quite insensitive to the selected parameters and their variations in the sensitivity studies except in the cases of the fuel gap dimension and the CHF correlation. With the doubled fuel gap dimension used in the code calculation,

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the resulted PCT is increased by 130 K in the comparison to that of the base case. In the sensitivity study of the Biasi CHF correlation, the reduction of the CHF does not yield improvement in the cladding temperature predictions at upper and lower elevations of the fuel rod. At the hottest location, significant reduction of the time-to-CHF is calculated with the reduction of the CHF, which leads to an overestimation of the PCT by more than 500 K.

From the results of the scenario study, it is learned that the present RELAP5/MOD2 model does not calculate the blowdown quench phenomena even at the assumption of connected flywheel system during the pump coastdown.

Excessive precursory cooling of the fuel rod is calculated during the reflood period. It is seen that discontinuities of the cladding surface heat flux and the vapor temperature are calculated at the moment of the reflood model actuation. Without using the reflood model in RELAP5/MOD2, the calculated cladding temperatures during the reflood period are in good agreement with the test data. These results may indicate that either the criteria used in RELAP5/MOD2 for the actuation of the reflood model calculation are inadequate or the heat transfer package in the reflood model is improper.

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1. INTRODUCTION

The assessment study documented in this report contributes to the overall code assessment effort, which is coordinated within the International Code Assessment and Applications Arr ram (ICAP) sponsored by the U.S. Nuclear Regulatory Commission (NRC). The objective of the ICAP is to provide qualitative assessment of the major thermal-hydraulic computer codes relative to code development, code improvement, and the enhancement of user guidelines. This report contains results from the best estimate experiment prediction analysis performed using the RELAP5/MOD2[1] Version 36.04 computer code to simulate the satem thermalhydraulic responses of the Loss-of-Fluid Test (LOFT) during Lossof-Coolant Experiment (LOCE) L2-5.

LOCE L2-5, in conjunction with previously conducted LOCE L2-2 and L2-3, is intended to evaluate the system responses during a large break loss-of-coolant accident (LOCA). These tests are conducted to address conservatisms in licensing criteria defined in the U.S. code of Federal Regulations (10CFR50 Appendix K). Current licensing criteria limit fuel rod cladding temperatures to 1,477 K (2,200 F). For most plants limited by this criteria, the peak cladding temperature occurs during reflood portion of the licensing calculation. While there are other limits that determine the maximum power a plant can oper-te at, the majority of plants are limited by the LOCA analysis.

Experiment L2-5 uses nominally the same system configuration as the previously performed Experiment L2-3. The essential differences between L2-5 and L2-3 are the post-break pump operation and ECCS actuation times. Experiment L2-2 and L2-3 unexpectedly show that during blowdown phase (with pump left running), a surge of coolant through the core occurs when flow from the pumps exceeds flow out of the cold-leg break. This coolant surge caused an "early rewet" of the nuclear fuel rods, effectively halting the rapid increase in cladding temperature that is typically predicted to occur in large break LOCAs. One purpose of Experiment L2-5 is to establish conditions which will result in a large break blowdown without "rewet". Therefore, in Experiment L2-5, the primary coolant pumps (PCPs) are unpowered quickly and then coast down while disconnected from their flywheel system. Such a coastdown during Experiment L2-5 is nontypical since the LOFT pumps would normally coast down while connected to their flywheel system to simulate the normal coastdown of the PCPs in a commercial PWR. The reason of having this nontypical PCP coastdown is the intention of producing core hydraulic conditions which would most likely prevent the early fuel-rod rewet that occurred during Experiment L2-3.

A RELAP5/MOD2 model used in the simulation of Experiment L2-5 is developed for the base case study according to the information provided by the Idaho National Engineering Laboratory (INEL). These information include description of the LOFT

facility [2], L2-5 test conditions [3], RELAP5/MOD1 input deck [4], and data report [5]. Except the base case study, sensitivity analyses with respect to various code input uncertainties are also performed to investigate their impacts on the calculation results, and to provide information in setting user guidelines of the RELAP5/MOD2 code. Scenario study on the pump coastdown behavior and simple modification of the CHF correlation in the code are made as well. In these studies, the experiment simulations using RELAP5/MOD2 begin with break initiation and subsequent blowdown, and continue through lower plenum refill, core reflood, and terminate with corewide quench.

This report is organized as follows: section 2 gives brief descriptions of the test facility and conditions. The RELAP5/MOD2 model used to simulate the experiment is described in section 3. In section 4 the calculation results compared to the test data are presented and discussed. Computational efficiency of RELAP5/MOD2 is given in section 5. Finally, some conclusions obtained from this study are drawn in section 6. A listing of the RELAP5/MOD2 input deck for the Experiment L2-5 simulation is provided in Appendix A.

2. FACILITY AND TEST DESCRIPTIONS

2.1 LOFT Facility

The LOFT facility is a 50-MWt pressurized water reactor system with instruments that measure and provide data on the

system thermal-hydraulic and nuclear core behavior during postulated LOCAs and anomalous transients. The LOFT facility consists of five major systems: reactor system, primary coolant system, blowdown suppression system, emergency core cooling system, and secondary coolant system.

The LOFT primary-coolant-system (PCS), shown in Figure 1.1, is volume-scaled to a typical four-loop commercial PWR. The general philosophy in scaling coolant volumes and flow areas in LOFT is to use the ratio of the LOFT core power (50 MWt) to a FWR core power (3,000 MWt).

The nuclear core of the LOFT facility is 1.68 m high and 0.6 m in diameter and contains 1,300 fuel rods and 4 control assemblies. A top view of the core arrangement is shown in Figure 1.2. The postulated broken loop and three unbroken loops of a four-loop PWR are simulated by a single broken loop and intact loop, respectively. The broken loop is connected to a suppression tank that holds the effluent and simulates the back pressure in a PWR containment building. The ECCS is designed functionally the same as commercial plant system but has additional flexibility in injection flow rates and locations.

The LOFT system response may not be identical to that of any specific commercial plant for a LOCA or operational transient. However, the LOFT design incorporates the same physical processes and general boundary conditions important to the transient so that results can be used to qualify the accuracy of the

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analytical models used for predicting accident behavior. The safety of commercial plants can then be assessed by these gualified models.

2.2 Experiment L2-5

LOCE L2-5 is the third experiment conducted in LOFT Power Ascension Experiment Series L2. The purpose of the LOFT L2 experiment stries is to provide thermal-hydraulic and fuel behavior data during double-ended cold-leg break experiments at various ECCS conditions. These data are to be used to evaluate and verify models in computer codes to predict large PWR LOCA response.

The major conditions achieved in Experiment L2-5 are: (1) the reactor has been operating at steady state power long enough to establish near equilibrium fission product concentrations; (2) there has been a loss of offsite power coincident with the LOCA, thus the primary coolant pump will be tripped off at break initiation and ECC injection will be delayed for a period of time corresponding to the delay until the commercial plant's emergency diesel is delivering power; (3) the minimum ECC action takes place, which requires that the High Pressure Injection System (HPIS), and Low Pressure Injection System (LPIS) flow rates be scaled to represent only one of the two pumps available for each system; and (4) The PCP will coast down without connection to its flywheel system in order to establish hydraulic condition which would prevent the occurrence of early rewet for this experiment. 2.2.1 <u>Initial conditions</u> Initial reactor criticality occurred about 54 hours prior to experiment initiation. The power level reached 36.0 + 2.0 MW 28 hours prior to Experiment L2-5 initiation, and was maintained at approximately that level until the experiment began. Prior to blowdown, the conditions in the intact loop were established to provide a flow of 192.4 + 7.8 kg/s, with temperature and pressure in the hot-leg of 589.7 + 1.6 K and 14.94 + 0.06 MPa, respectively.

2.2.2 Experiment procedure The experiment was initiated by opening the Quick Opening Blowdown Valves (QOBVs) in the broken loop hot-leg and cold-leg. The reactor scrammed on low pressure at 0.24 + 0.01 s. Following the reactor scram, the operators tripped the PCPs at 0.94 + 0.01 s. Accumulator injection was actuated when the system pressure dropped below 4.2 MPa. Delayed ECC injection from the HPIS and LPIS were actuated at 23.90 + 0.02 and 37.32 + 0.02 s, respectively. The LPIS injection was stopped at 107.1 + 0.4 s, after the experiment was considered complete.

3. CODE AND MODEL DESCRIPTIONS

3.1 Computer Code

The RELAP5/MOD2 Version 36.04 computer code is used to simulate the transient thermal-hydraulic response of the LOFT system during Experiment L2-5. RELAP5/MOD2 is a one-dimensional, two fluid, six-equation, thermal nonequilibrium reactor transient

and accident analysis program. This computer code is developed at the INEL for the U.S. Nuclear Regulatory Commission. Specific application of the code to the Experiment L2-5 simulation is discussed in the following sections.

3.2 Model Descriptions

The RELAPS/MOD2 model of the L2-5 simulation is shown in Figure 3.1. The nodalization used in this study is based on the nodalization presented in Reference 4 with changes where necessary to convert the RELAP5/MCD1 model into the RELAP5/MOD2 model and to make simplification based on experience obtained in using of the code. This mo consists of 128 volumes, 145 junctions, and 77 heat structures to describe the LOFT systems including reactor vessel, broken loop, intact loop, pressurizer, steam generator, and ECCS. Brief descriptions of til RELAP5/MOD2 model of the LOFT facitily are presented as follows.

3.2.1 <u>Reactor vessel</u> The reactor core is represented by two parallel six-volume channels --- hot and average channels. The geometry of the hot channel represents that of the center fuel assembly in the LOFT core; the average channel is used to simulate the remaining eight fuel assemblies. Crossflow junctions with appropriate flow areas and resistances between volumes are employed to represent the interconnections of these assemblies. A three-section pipe in parallel with fuel channels is used in modeling the bypass channel.

Modeling of the reactor vessel downcomer is one area of major importance in a large-break LOCA analysis because of ECC water injection phenomena. Conventionally, the downcomer was modelled by a single series of vertically stacked control volumes. The inadequacy of this model was demonstrated in the LOFT large-break LOCA simulations in which strong azimuthal asymmetries were measured, especially during ECC injection. The conventional downcomer model apparently is unable to calculate these phenomena. This deficiency can be improved by modeling the downcomer as a two-channel downcomer interconnected with crossflow junction. In this study, the downcomer is split into two equal parts (with equal flow area and volume) associated with the intact loop and broken loop, respectively. Each part is represented by six stacked annulus components. The connections between the parallel downcomers are represented by crossflow junction.

The lower plenum and upper plenum are divided into several control volumes and simulated by branch or single-volume components in the RELAP5/MOD2 model.

Cylindrical heat structures are included to represent highpowered fuel rods (4 rods in the core center) and average fuel rods in the hot channel, and average fuel rods in the average channel. These heat structures representing the fuel rods are each divided vertically into six geometrical structures to allow different radial nodalization dimensions of the fuel rods at

different axial locations associated with different power levels. The best estimate values of the dimensions of the fuel pellet, gap, and cladding corresponding to the Experiment L2-5 power levels are used in order to obtain the best estimate initial stored energy. Reflood option is chosen for the fuel rod heat structures, and reflood calculation will be turned on when the connected hydrodynamic volume is nearly empty. A maximum number of axial fine mesh intervals of 8 is specified for axial length of 0.28 m during reflood calculation.

Other heat structures representing the flow ducts and reactor vessel are also modelled to describe the appropriate heat transfer between different flow channels, and ambient.

3.2.2 <u>Broken loop</u> Modeling of the broken loop deserves careful attention since the accuracy of the break flow calculation is of major importance in the predictions of the system responses of a large break LOCA. In this study, the broken loops (hot-leg and cold-leg) are simulated by a series of branch and pipe components, and the QOBVs are represented by trip valves to simulate the break junctions. Downstream of the break junctions, the broken loops are connected to time-dependent volumes where the pressure boundary conditions of the blowdown suppression tank (BST) are provided. Flow areas and flow resistances of the junctions along the broken loops are specified to simulate the pump simulator, steam generator simulator, and broken loop piping. Choked-flow model is applied to the junctions wherever the junction flow area is restricted.

Definition of the break geometry is also of importance in accurately calculating the break flow. A discharge coefficient is required to account for multi-dimensional effects at the break that cannot be calculated using one-dimensional computer codes. A recommended discharge coefficient of 0.84 [6,7] is applied in the broken loop cold-leg break for both subcooled and saturated choked flow. However, a discharge coefficient of 1.0 is used for the broken loop hot-leg break.

3.2.3 Intact loop The intact loop modeling includes the hot-leg, loop seal, PCP, and cold-leg which are simulated by branch, single-volume, pipe, and pump components. Pump characteristics (head curves and torque curves) are provided for single-phase conditions. A set of two-phase diff ance curves are input, in conjunction with the single-phase curves are input, in phase pump performance. The moment of luertia of the pump rotor shaft (1.43 kg-m) is used to characterize the coastdown behavior of the PCP.

3.2.4 <u>Pressurizer</u> The pressurizer model is not expected to be sensitive to the calculated peak cladding temperature in a large break LOCA analysis, therefore, simplification with neglecting the water spray and heater is made in order to save computation effort. The pressurizer surge line is nodalized with three control volumes and related junctions. The pressurizer tank is

represented by a seven-section pipe with PORV simulated by a trip valve connecting to a time-dependent volume with atmospheric pressure at the top.

3.2.5 <u>Steam generator</u> The steam generator primary side is represented by two branch components in modeling of the inlet and outlet plena, and an eight-section pipe (with four sections direct vertically upward and four sections direct downward) in simulating the steam generator U-tubes. In the secondary side, it is represented by a series of feedwater system, downcomer, boiler, seperator, riser, and mist extractor simulations based on various components available in the RELAP5/MOD2 code. At the exit of the secondary side, # time-dependent volume is used to provide the pressure boundary conditions of the air-cooled condenser. Cylindrical heat structures representing the tubes are added to permit the heat exchange between the primary and the secondary sides of the steam generator. Additional heat structures are also used to simulate the heat loss to the environment.

3.2.6 ECCS The emergency core cooling systems, including the accumulator, HPIS and LPIS are simulated in the RELAPS/MOD2 model. The accumulator is represented by an ACCUMTOR component with back pressure of 4.2 MPa. The HPIS and LPIS are modelled by time-dependent junctions with injected coolant flow controlled by the system pressure. In order to simulate delayed HPIS and LPIS established in L2-5 test, the HPIS and LPIS are initiated in the calculation model at given times (23.9 and 37.32 s, respective-

ly). The accumulator flow is, however, actuated when the calculated system pressure drops below its back pressure, and the accumulator flow rate is determined by the pressure difference and given flow resistance. All emergency coolant injections are conducted to a common volume (volume 600) before being injected to the intact loop cold-leg.

Downstream of the accumulator, a TRPVLV component (junction 603) is used in simulating the accumulator check valve. This component will be used to shutoff nitrogen injection after the accumulator is empty in order to avoid the numerical problem of the RELAP5/MOD2 calculation.

3.3 Initialization Process

The RELAP5/MOD2 model of the L2-5 experiment simulation is initialized to a steady-state corresponding to the test initial conditions before it is utilized for the large break LOCA transient analysis. During initialization, the following processes are taken:

(1) In order to achieve pressure condition, a time-dependent volume with system initial pressure (14.94 MPa) is connected to the top of the pressurizer _ank.

(2) In order to obtain correct pressurizer water level (i.e. primary water inventory), a tirt-dependent volume is connected to the bottom of the pressurizer tank by a time-dependent junction. The flow rand (including both insurge and outsurge flows) of the time-dependent junction is controlled by the difference between

the calculated water level and desired water level. Thermodynamic properties of the water inventory provided by the time-dependent vol me are specified according to the properties of the water in the pressurizer tank.

(3) In the primary coolant system, minor adjustments of the flow resistances at certain locations are made in order to achieve the flow condition and core T.

(4) At the steam generator secondary side, a pressure lower than the measurement is used in the RELAP5/MOD2 model in order to obtain the primary coolant temperature closing to the test data. This requirement shows a possible deficiency of RELAP5/MOD2 in describing heat transfer between the primary and the secondary sides. However, the conditions of the steam generator secondary side is not sensitive in determining the system response of a large break LOCA type of transient, minor adjustment of the secondary side pressure is acceptable.

The initial conditions of the RELAP5/MOD2 model obtained by the initialization process are listed in Table 3.1 in comparison to the test data.

4. RESULTS AND DISCUSSIONS

Results of the experimental simulation of the thermalhydraulic responses of L2-5 test are assessed through comparison of experimental data. The comparisons presented in this report

are representative key parameters of the L2-5 large break LOCA transient.

4.1 Base Case Analysis

Following the test procedure in L2-5 simulation with transient calculation initiated by the opening of break valves, the timings of major events calculated by RELAP5/MOD2 compared to the test data are listed in Table 1.1. There is no significant difference between the calculated transient scenario and the test result.

The calculated pressure response upstream of the cold-leg break (volume 345) compared to the test data are shown in Figure 4.1. An extremely rapid system depressurization commences with the opening of the QUBVs. Figure 4.1 shows that both the calculated and measured pressures drop from 14.94 MPa to 10.0 MPa immediately after the test initiation. As the pressure decreases, the temperature of the liquid in the vessel reaches saturation and flashing phenomenon occurs. Consequently, the depressurization rate is reduced by the voiding in the vescel as shown in both the calculation result and test data. The calculated pressure closely follows the test data at the first five seconds. After that, the pressure is underpredicted by RELAP5/MOD2 with little difference to the measurement. In Figure 4.2, the comparison of the pressurizer pressure is shown. It can be seen that the differences between the calculated and measured pressures are large with lower pressurizer pressure being

calculated by RELAP5/ MOD2. This could be resulted from the overprediction of the outsurge flow and the neglect of the pressurizer heat structure in the calculation model. The inflection point of the pressurizer pressure response at the mom nt of pressurizer empty occurs earlier in the calculation than that of measurement. According to the pressurizer water level response shown in Figure 4.3, the calculated pressurizer empty occurs at 10.0 s after the test initiation, which is about four seconds earlier than the test data.

In Figure 4.4, calculated interfacial water levels of the core region, the downcomer region near intact loop, and the downcomer region near broken loop are shown with level zero referring to the botton of the reactor vessel. Based on the calculated water level in the core region, the L2-5 large break LOCA transient is divided into three periods: blowdown phase (0 to 21 s), refill phase (21 to 30 s), and reflood phase (30 to 54 s). According to the void : asurements of L2-5 test, lower plenum refill starts at 22 s and ends with the begining of core reflood at 31 s; and core reflood sequentially completes at 55 s. These events and their timings are well predicted by RELAP5/MOD2. During the blowdown phase, the calculated water level at the downcomer near broken loop declines much faster than that of the downcomer near intact loop. This result emphasizes the necessity of the downcomer modeling used in this study. In the core region, an even faster water level decrease is calculated with minimum

water level reaching 0.623 m below the bottom of the active fuel at 21.3 s. At this time, the blowdown phase of the transient ends and the refill phase begins as liquid from the accumulator reaches the lower plenum. The lower plenum is then refilled when the calculated water level reaches the bottom of the active fuel at 30.5 s. The end of the core reflood is calculated when the water level reaches the top of active fuel at 54.0 s. During the reflood period, the calculated water level rises with a rate of 70 mm/s.

Figure 4.5 shows calculated mass flow rates from the accumulator, HPIS, and LPIS. Calculated HPIS and LPIS flow rates shown in this figure are 1.585 kg/s and 6.42 kg/s, respectively. Compared to the test data, calculated HPIS and LPIS flow rates are overpredicted (measured HPIS and LPIS flow rates are 0.75 kg/s and 6.0 kg/s, respectively) because of the underprediction of the system pressure by RELAP5/MOD2. Since the major portion of the ECC flow is provided by the accumulator, the differences found in HPIS and LPIS flow rates can be neglected. The calculated accumulator flow initiated at 15.7 s goes up to 50.0 kg/s at 27.7 s, and then decreases linearly to 30.0 kg/s at the end of the calculation (90.0 s). However, the accumulator flow is, unfortunately, failed to be measured in L2-5 test. After the actuation of the accumulator recorded at 16.8 s, the only available measurement regarding to the accumulator is the accumulator water level, which gives an indication that the

Account 24.00 r flow ends at 50.0 s because the water level drops flow the inlet of the variable standpipe at that time. In L2-5 cest, the inlet of the variable standpipe is located at 0.95 m above the bottom of the accumulator tank. Therefore, certain amount of water (about 1,200 kg) stored below the variable standpipe inlet would not be injected into the reactor vessel. This condition is not included properly in the calculation model of the base case study which consequently leads to a continuous accumulator flow after 50.0 s in the calculation result. This error may not be significant in calculating the L2-5 transient since major events are almost complete at that time. A sensitivity study with accumulator tripped off at 50.0 s will be performed to investigate whether it is important or not in calculating the L2-5 transient.

According to the test data, single-phase blowdown ends and two-phase blowdown begins at the cold-leg break 3.4 s after the experiment initiation. While in the calculation, break flow transition from subcooled to saturated condition occurs at 2.0 s. Calculate³ cold-leg break flow rates compared to the test data are shown in Figure 4.6. It is seen that RELAP5/MOD2 gives good result in the prediction of the cold-leg break flow during the blowdown period. In general, subcooled break flow is slightly underpredicted while saturated break flow is overestimated by the RELAP5/MOD2 model. During the refill and reflood periods, RELAP5/MOD2 calculates an almost zero break flow while the test

data shows a bunch of water slugs periodically rush out of the cold-leg break. The cold-leg break flow observed during the refill and reflood periods of L2-5 test may be attributed to the ECC bypass which is not calculated by the RELAP5/MOD2 model. Certainly, the underprediction of the system pressure shown in Figure 4.1 could be the reason of the underestimation of the break flow during these periods. After 70.0 seconds, increased cold-leg break flow rates are calculated because the calculated downcomer water level increases to the level of the cold-leg break by the excessive accumulator flow.

For the hot-leg break flow comparison shown in Figure 4.7, significant differences are .ound during the blowdown period. However, the calculated break flow shows excellent agreement with the test data later on. During blowdown, the measured flow rate shows a hump shape response while the calculated break flow monotonically decreases from its initial peak value. It is seen that the measured flow rate drops from an initial flow of 210 kg/s to a minimum flow of 30 kg/s at 4.0 s, and then increases to a maximum flow of 70.0 kg/s at 8.0 s. During this period, the break flow is significantly overpredicted by the RELAP5/MOD2 model. In the test data, the reason for the break flow to increase during system depressurization is very difficult to identify without other detailed measurements. The break flow can be increased with the increasing density (or with the decreasing void fraction) near the break. Probably, the break flow increase

as observed in L2-5 is due to "loop clearance" occurred at the top of the steam generator simulator. During the blowdown period, bubbles are generated by flashing flow upward along the U-tube (0.367 m ID pipe) of the steam generator simulator. Because the broken loop flow is restricted by the critical discharge at the break, the flowing bubbles could be momentarily accumulated in the region of the U-tube bend which results in a vertical stratification pattern in the U-tube pipe. At the moment when the broken loop cold-leg starts voiding, the cold-leg break flow rate is suddenly reduced which produces a perturbation to push the upstream liquid in the broken loop hot-leg over the U-tube bend. This liquid push over will yield consequently a syphon phenomenon which leads to void reduction near the break and therefore the hot-leg break flow increases. Calculated void fractions near the breaks are shown in Figure 4.8. From this figure, it is noted that the broken loop hot-leg starts voiding immediately after the break initiation. Small oscillation of the hot-leg void are calculated during the period of 4.0 to 8.0 s resulted from the occurrence of significant void in the broken loop cold-leg. The hot-leg void oscillation leads to oscillation of the hot-leg break flow without having flow increase in the calculation results. The failure in the prediction of the hotleg break flow increase during blowdown with the RELAF5/MOD2 code could refer to its capability in the modeling of the phase seperation and loop clearance phenomena.
The mass flow rate of the intact loop cold-leg is shown in Figure 4.9. Before the accumulator flow initiation, the cold-leg flow calculated by RELAP5/MOD2 agrees reasonably well with the test data. Flow oscillation observed in L2-5 after ECC injection due to direct contact condensation is also calculated by RELAP5/MOD2 with smaller oscillation magnitude than the test data.

The comparison between calculated and measured results of the intact loop hot-leg flow is shown in Figure 4.10. Significant discrepancies of the flow rates during the blowcown period are found in this figure. In order to understand the differences, a more detailed comparison of the hot-leg flow during the blowdown period is presented in Figure 4.11 with zero flow indication. It clearly shows that calculated flow rates are lower than the test data at the first few seconds of the initial period. After four second f the transient, negative flow rates (water runback) caused by the PCP stop are calculated with similar magnitudes of the positive flow rates shown by the test data. It is known [5] that as the result of partial failure of the flow measurement in test L2-5, the test data provides only the magnitude of the intact loop hot-leg flow without indication of the flow direction. However, the differential pressure measurement across the intact loop hot-leg indicates the existence of reverse flow during the bl fown period because the measured differential pressure changes sign from an initial

positive value to . negative value at 5.0 3, and maintains negative pressure difference to the end of the blowdown period.

Calculated core flow rates during the blowdown period are shown in Figure 4.12. It shows that the core inlet flow changes direction immediately after the break initiation from a positive (upward) flow of 195 kg/s to a negative (downward) flow of 250 kg/s, while a positive flow is sustained at the core outlet for 0.5 s. This bidirectional flow configuration results in the reducing of water inventory in the core region, flow stagnation somewhere in the core, and the occurrence of transient CHF. Core flow oscillation induced by direct condensation during ECC injection is also calculated and presented in Figure 4.13.

Calculated cladding temperatures of the hot channel hot rod at different axial elevations (with level 1 corresponding to the bottom node) are shown in Figure 4.14. It is seen that significant temperature rises are calculated for the fuel rod cladding at levels 2, 3, and 4 when CHF conditions are predicted at 0.3 s. At the level 1 position, temperature spikes occur with relatively small magnitudes during the blowdown and refill periods. At higher portions of the fuel rod (levels 5 and 6), calculated cladding temperatures keep going down without departure from saturation temperature during the whole transient. However, the cladding temperature measurements located at various axial positions from the bottom to the top of the hottest fuel rods indicate that the whole fuel rods experience CHF during L2-5

test. Inaccurate predictions of the cladding temperature responses at the upper and lower parts of the fuel rod could be resulted from inaccurate prediction of the CHF. The present model used in RELAPS/MOD2 for CHF calculation is the Biasi correlation which overpredicts the CHF by 60% in the comparison to the dryout experiment conducted at the Royal Institute of Technology in Sweden [8]. A sensitivity study with reduced Biasi CHF will be performed to see whether the cladding temperature prediction can be improved.

In test L2-5, a peak cladding temperature (PCT) is recorded at one third of the full length of the fuel rod from the bottom which corresponds to the elevation at the middle of the level 2 and level 3 positons in the calculation odel. However, differences in calculated cladding temperatures between the level 2 and level 3 positions are small. Therefore, calculated cladding temperatures of the level 3 elevation shown in Figure 4.15 are used in the comparison to the test data. According to the calculated cladding temperature response, the CHF occurrence is predicted at 0.3 s after the break initiation. The calculated cladding temperature reaches a peak value of 1,112 K at 7.0 s and sustains at that level to the end of the blowdown period without the occurrence of the early fuel rod rewet. An enhanced cooling is calculated after the reflood model is turned on at 26.0 s, which depresses the cladding temperature to a calculated guench temperature (T) of 530 K at 57.2 s. In test L2-5, the cladding

temperature drops before the CHF occurs at 0.9 s. After that, a severe heatup of the fuel rod cladding is detected, and the cladding temperature increases from 600 K to 1,000 K in six seconds. A slower temperature increase is then measured to the end of the refill period with the PCT of 1,077 K reached at 28.5 s after the experiment initiation. Early quenching phenomena observed in test L2-3 does not occur in test L2-5 because different hydraulic conditions achieved in these tests. At the begining of the reflood period, the measured cladding temperature starts declining with slower decreasing rate than that of the calculated temperature. Fuel rod guench occurred at 54.0 s is detected when the cladding temperature drops to 820 K which is about 300 K higher than the RELAP5/MOD2 calculation. The underestimation of the fuel rod quanch temperature by RELAP5/MOD2 is also found in the comparison to FLECHT-SEASET data [9]. It is caused by a simplified formula in computing quench temperature currently used in the reflood heat transfer package which gives an almost constant guench temperature of 520 K [1]. Based on the observation of the guench temperature in test L2-5, the calculation model should be reexamined.

The underprediction of the cladding temperature before quench caused by an excessive cooling is calculated with the reflood model of RELAP5/MOD2. Currently, the reflood model uses a correlation for the dispersed-flow film boiling heat transfer based on Dougall and Rohsenow's modifications to the single phase

flow Dittus coelter correlation. It is known that the correlation does not account for nonequilibrium effect, therefore, tends to overpredict the film boiling heat transfer coefficients [10,11].

The excessive precursory cooling of the fuel cladding by the RELAP5/MOD2 calculation could also be caused by excessive interfacial drag with its present model [12,13]. Too much liquid is entrained from the lower plenum to the core region. In the hydraulic volumes next to the fuel where post-dryout condition occurs, the flow regimes predicted by RELAP5/MOD2 are mist (dispersed) flow during the refill and reflood periods. Increased liquid droplet entrainment will increase interface heat transfer area between the liquid and vapor, which in turn will reduce the degree of vapor superheating in rod bundles and lead to a higher driving potential for energy removal. In addition, the vapor superheating could be also underpredicted by RELAP5/MOD2 with its present interfacial heat transfer model at high void flow conditions [14,15]. Moreover, steep increase of the wall heat flux is calculated at the moment of the reflood model actuation, which contributes also to the excessive precursory cooling. Detailed discussions of the reflood model calculation can be seen in the following section.

Evidence of RELAP5/MOD2 underpredicting the vapor superheating can be observed from the comparison of fluid temperatures at the upper plenum and hot-leg, Calculated fluid temperatures at the upper plenum (volume 240) compared to the test data are shown

in Figure 4.16. The temperature measurements indicate the existence of superbeated steam while calculated temperatures show that both the liquid and vapor stay saturated during the refill and reflood periods. At the end of the reflood period, subcooled ECC water reaching the upper plenum region is calculated. Superheated vapor is also observed in the hot-leg region during L2-5 test. Fluid temperature responses at the intact loop and broken loop are shown in Figures 4.17 and 4.18, respectively. Again, the comparison clearly indicates that RELAP5/MOD2 fails in calculating the extent of vapor superheating of the L2-5 transient.

In the intact loop cold-leg, near the ECC injection point, subcooled liquid temperatures are calculated at the moment of the accumulator flow initiation. According to the measurements shown in Figure 4.19, the thermocouple could be surrounded by vapor space at the initial period of the accumulator injection, subcooled temperature is detected with several seconds delay. Temperature oscillation measured during the accumulator injection can be caused by the alternate contact of the liquid and vapor phases with the thermocouple. However, measured fluid temperature in the intact loop cold-leg is higher than the RELAPS/MOD2 prediction. The underprediction of the liquid temperature could be resulted from underestimation of the condensation with the RELAPS/MOD2 model.

In the downcomer region, calculated liquid temperatures of the upper portion (volume 202 and 282) and the lower portion

(volume 210 and 290) are shown in Figures 4.20 and 4.21, respectively. It is seen that calculated temparatures near the intact loop where ECC water is injected are different from that near the broken loop. At the intact side, the delivery of the subcooled ECC water to the downcomer is calculated with few seconds delay after the accumulator flow initiation. At the broken side, subcooled liquid temperature is calculated in the downcomer when the liquid level increases during the refill and reflood periods. In test L2-5, downcomer fluid temperature measurements are located at an azimuthal angle of 155 away from the intact loop cold-leg. The fluid temperature responses measured at various axial locations in the downcomer region are shown from Figures 4.22 to 4.25 for the comparison to the calculated temperatures in the downcomer near the broken loop. The temperature underprediction shown in these figures could be caused by the underprediction of the heat transfer between the vessel hot wall and the ECC liquid. Of course, the downcomer liquid temperature could be also underpredicted if the ECC condensation is underestimated with the RELAP5/MOD2 model.

The comparison of the fluid temperatures of the broken loop hot-leg is shown in Figure 4.26. Significant differences found fter 60.0 s are caused by the excessive accumulator injection in the calculation model.

The comparisons of the fluid densities of the intact loop cold-leg, intact loop hot-leg, and broken loop cold-leg are

presented in Figures 4.27, 4.28 and 4.29, respectively. Calculated fluid densities in the intact loop cold-leg /gree well with the measurem ts before the actuation of the accumulator. Increased densities with ECC injection are noted in the test data with significant variations resulted from local measurement. In the calculation results, the volume-averaged densities are shown with smooth changes. Density overprediction in the RELAP5/MCD2 calculation after 60.0 s is due to overfill of the downcomer by excessive accumulator flow. Excessive carryover of the core liquid to the intact loop hot-leg is illustrated by the high density fluid present after 45.0 s (see Figure 4.28). The cause of this carryover lies in the interfacial drag model used in the RELAP5/MOD2 code. In the broken loop cold-leg (volume 345), calculated densities shown in Figure 4.29 are in good agreement with the test data during early period of the transient. After about 10.0 s, calculated densities in general are higher than the measurements. It is interesting to note that the calculated density in the broken loop cold-leg is high while the calculated cold-leg break flow shown in Figure 4.6 is almost zero during the EC. injection period. The questions turn out to be where the high density fluid comes from and where it goes during the refill and reflood periods. In Figure 4.30, calculated mass flow rates of the BLCL junction (vessel outlet junction from volume 282 to volume 335) and the cold-leg break junction are shown. From this figure, it is seen that fluid periodically flows into the broken

loop cold-leg and back to the reactor vessel without exiting flow through the break during 25.0 to 42.0 s. However, whether the flow is provided by the carryover from the downcomer or resulted from the ECC bypass phenomena in the calculation model remains unknown. Calculated flow rates of the BLCL junction are compared to that of junction 272 and junction 283 in Figure 4.31. A positve flow of the junction 272 represents bypass flow from the intact side (volume 202) to the broken side (volume 282); while a negative flow of the junction 283 indicates the amount of carryover from downcomer to the broken loop. It is seen from Figure 4.31 that in general the junction 272 flow is less than zero, i.e. reverse flow is calculated on the flow path of the ECC bypass. It is known that the ECC bypass phenomena will occur when the ECC water can flow downward the annulus downcomer by gravity and be swept out through the break by the iscaping upward steam flow, that is, due to the counter-current flow limitation (CCFL) phenomenon. However, there is no direct modeling of the CCFL in RELAP5/MOD2, and the existing model of the interfacial drag is not good enough in retarding the downflow of the ECC water [16]. Therefore, it can be concluded that the RELAP5/MOD2 model does not calculate ECC bypass in the L2-5 simulation. High density fluid of the broken loop cold-leg during ECC injection is resulted from excessive carryover with the present RELAP5/MOD2 models.

4.2 Sensitivity Studies

In addition to the base case calculation, sensitivity studies are performed to explore the effects of input modeling and code options. Scenario study and simple model modification, specifically speaking, the pump coastdown behavior and the Biasi CHF correlation are also analyzed in elucidating the code performance. The identifications of the cases analyzed in this study are listed in Table 4.2 with the conditions which are different from that of the base case. The purpose and the results of the sensitivity studies are discussed in the following sections.

4.2.1 <u>ACCUM50</u> This case study is used to identify the influences of the thermal-hydraulic response predictions resulted from the excessive accumulator flow of the base case. Calculated accumulator flows compared to the base case are shown in Figure 4.32. The water level comparisons are presented from Figure 4.33 to 4.35. Major differences of the water level responses can be seen when the accumulator flow is tripped off at 50.0 s in the ACCUM50 case. The cold-leg break flow shown in Figure 4.36 indicates similar results except some flow spikes after 70.0 s are calculated. Calculated fluid densities of the broken loop cold-leg are compared in Figure 4.37. Simulation with correct accumulator flow stop can improve the prediction of the density at later period. However, the calculated density of the ACCUM50 case is still higher than the test data. In Figures 4.38 and

4.39, calculated cladding temperatures are shown. It is seen that there is no significant difference in the cladding temperature prediction resulted from the difference in the accumulator simulation. With lower accumulator flow simulated in the ACCUM50 case, the fuel rod quench is delayed by 2.0 seconds compared to the base case.

4.2.2 <u>BLHL-HT</u> In the base case study, it is found that the hotleg break flow is overpredicted during the blowdown phase. Considering the possible uncertainties in the temperature measurements, higher initial temperatures of the broken loop hotleg are used in the BLHL-HT case to see if the hot-leg break flow prediction can be improved.

Reduced hot-leg break flow with the increasing of the initial temperature is shown in Figure 4.40. However, the hump shape of the break flow response shown by the test data is still failed to be calculated. With reduced hot-leg break flow, increasing of the cold-leg break is expected. Figure 4.41 shows that the calculated cold-leg break flow of the BLHL-HT case is higher than the base case in the first two seconds. Cladding temperature responses at various axial locations are compared in Figure 4.42. Significant difference is seen in the cladding temperature at level 2 position. This could be resulted from the relocation of the stagnation point. Higher flow resistance can be induced by the higher initial temperature in the broken loop hot leg, which moves the stagnation point upward in the core

region and introduces an increaced reverse flow in the level 2 node immediately after the opening of the QOBVs. The increased reverse flow will then prevent the deviation from saturation at that location. However, the calculated PCT at the hottest location (level 3) of the BLHL-HT case is only 20 K lower than that of the base case (see Figure 4.43).

4.2.3 <u>BLHL-DC</u> The calculated flow can be reduced with reducing of the discharge coefficient specified in the RELAP5/MOD2 input. In the BLHL-DC case, the hot-leg break dischage coefficient is reduced from 1.0 in the base case to 0.8.

It is seen from Figure 4.44 that the calculated hot-leg break flow is decreased by this input change, but with limited difference from the base case. The other parameters, including the pressure, cold-leg break flow, and cladding temperature responses, shown in Figures 4.45 to 4.48 indicate minor effects of the hot-leg break discharge coefficent on the L2-5 simulation. 4.2.4 <u>BLHL-5K</u> Regarding the uncertainty of the form loss coefficient during flow transient condition, a sensitivity study is needed to investigate the possible impacts in the large break LOCA calculation. In the BLHL-5K case, the form loss coefficents of the junctions in the broken loop hot-leg specified in the RELAPS/MOD2 input are five times of the base case.

Calculated pressures of the broken loop cold-leg and pressurizer compared to the test data are shown in Figures 4.49 and 4.45, respectively. It is seen that the system pressure

increases with increased form loss coefficient in the broken loop hot-leg. During the blowdown period, the calculated pressure of the broken loop cold-leg is higher than the test data with increased form loss coefficient, however, the calculated pressure of the pressurizer is still much lower than the test data. Significant reduction of the hot-leg break flow is seen in the BLHL-5K case (see Figure 4.51). In general, better agreement on the hot-leg break flow is seen in the BLHL-5K case, but the initial break flow is apparently underestimated. Because of the increasing of the system pressure, the calculated cold-leg break flow shown in Figure 4.52 is increased with the increasing of the form loss coefficent. The comparisons of the cladding temperatures are presented in Figures 4.53 and 4.54. The major difference is found in the temperature response of the level 2 position as resulted from the relocation of the stagnation point. The fuel guench time is delayed by 8.0 seconds while the PCT is compatible in the comparison to the base case.

4.2.5 <u>PV-X-PL</u> The RELAP5/MOD2 numerical scheme is generally formulated using one-dimensional elements. However, there are several applications where an approximate treatment of crossflow provides an improved physical simulation. One major application of the crossflow junction is to provide a tee model. In the L2-5 base deck, the pressure vessel outflow junctions connecting to broken loops are considered to be normal junctions. In reality, the momentum flux in the reactor vessel is perpendicular to the

momentum flux in the broken loop. Therefore, crossflow junctions instead are chosen in the PV-X-BL case to identify the difference with this option in the L2-5 simulation.

Important parameters with respect to the large break LOCA transient, including the break flows and cladding temperatures, are shown in Figures 4.55 to 4.58. It is interesting to see the calculated break flows, both in the hot-leg break and the coldleg break, with crossflow junction modeling are equal to the base case. The effects of the crossflow option on the cladding temperature responses are calculated with limited differences. The PCT calculated in the PV-X-BL case is the same as that of the base case.

4.2.6 <u>MESH\$32</u> A fine mesh-rezoning scheme is implemented to efficiently use the two-dimensional conduction solution for reflood calculations. It is suggested in the RELAP5/MOD2 manual that appropriate user-specified maximum number of axial fine mesh intervals is 8 to 32 with the length of hydrodynamic volumes ranged from 0.15 m to 0.6 m. In the analysis of the MESH#32 case, the number of fine mesh intervals increases from 8 used in the base case to 32.

The results of this study are presented in Figures 4.59 to 4.62. It is seen that important paramters calculated with increased number of fine mesh intevals are identical to those in the base case, except a little difference of the fuel quench time.

4.2.7 <u>FUEL-GAP</u> It is well known that fuel gap distance (or gap conductance) is an extremely important parameter in determining the PCT during a large break LOCA. In the L2-5 base deck, varied fuel gap distances are used for various axial and radial locations of the fuel rods in accordance with different power levels. At the hottest section, the fuel gap distance specified in the base deck is 0.04944 mm. In the FUEL-GAP case, a mominal fuel gap distance of 0.0953 mm [2] is universally used for fuel rod modeling at various locations. The increase of the fuel gap distance will reduce the gap conductance and, consequently, increase the initial rod temperature and the initial stored energy.

Radial profiles of calculated rod temperatures at the hottest location are presented in Figure 4.63. It is seen that the initial fuel rod centerline temperature of the FUEL-GAP case is 270 K higher than the base case. The effect of the increased stored energy on the cladding surface temperature can be seen in Figures 4.64 and 4.65. The PCT calculated for the FUEL-GAP case is 130 K higher than that of the base case in the L2-5 simulation. This disparity emphasizes the importance of fuel-rod modeling for the large break LOCA transient analysis. Calculated break flows presented in Figures 4.66 and 4.67 are, however, not affected by the increasing of the fuel gap distance.

4.2.8 <u>PUMP-FW</u> The major difference observed between the LOCE L2-3 and L2-5 tests is the early rewet phenomena as a result of

different operations of the primary coolant pumps during the transients. In the base case study, no early rewet of the fuel rod is calculated according to the pump operation of L2-5. In a sensitivity study [41 performed with earlier version RELAP5/MOD1, it is found that the early rewet of the fuel rod can be predicted in the L2-5 simulation if the pumps coast down with their flywheel system. In this study, the same assumption on the pump behavior is used to see whether the RELAP5/MOD2 code can predict early quenching.

Figure 4,68 shows the coolant mass flow rate of the intact loop cold-leg provided by the surge flow from the coastdown pump. It is seen that with the assistance of the flywheel system the cold-leg flow of the PUMP-FW case is sustained for a longer period than the base case. Because of the higher coolant flow in the intac' loop cold-leg of the PUMP-FW case, a positive core flow is re-estabilished at earlier time and results in a higher core flow between 5.0 to 10.0 s in the comparison to the base case (see Figure 4.69). However, calculated cladding temperature shown in Figure 4.70 indicates no early rewet even though the pumps coastdown with their flywheel is assumed in the calculation. Calculated cladding temperatures of the PUMP-FW case deviate from the base case after 7.0 s with small difference. The calculated PCT of the PUMP-FW case is almost the same as that of the base case. Calculated break flows shown in Figures 4.71 and 4.72 can be used to illustrate the insignificant

effect of the pump coastdown behavior on the break flow calculation in the L2-5 simulation.

4.2.9 <u>CHF*0.6</u> Regarding the failure of the cladding temperature predictions at the upper and lower portions of the hottest fuel rods in the base case study, the accuracy of the Biasi CHF correlation used in RELAP5/MOD2 is guestioned. This sensitivity study is performed with a modified Biasi correlation (simply multiply by a factor of 0.6) to see whether the cladding temperature prediction can be improved.

Results of the cladding temperatures are shown in Figures 4.73 to 4.75. It is learned that the discrepancies of the cladding temperature responses at the upper portion of the fuel rod found in the base case still exist in the CHF*0.6 case. The calculation model still fails in predicting CHF at low power sections. Moreover, the predictions of the cladding temperatures of the hottest portion are even worse with the CHF reduction. In Figure 4.73, it is seen that the time-to-CHF is reduced from 0.3 s in the base case to almost time zero with the reduction of the CHF, and the associated PCT is calculated to be 500 K higher than the test data. Therefore, a solid statement on the Biasi correlation can not be made, and the reason for the failure of the cladding temperature prediction is unknown.

4.2.10 <u>NORFLOD</u> Different heat transfer correlations are used in RELAP5/MOD2 for post-dryout condition between the calculations with and without reflood model option [1]. The reflood model

calculation is actuated when the system pressure is lower than 1.0 MPa, when the mass flux is less than 200 kg/m s, all when the connected hydrodynamic volume is nearly empty. In view of the failure of the cladding temperature prediction resulted from the excessive precurso. cooling during the reflood period of the base case analysis, an experimental simulation is performed without the actuation of the reflood model in the RELAPS/MOD2 calculation.

Calculated void fractions in the hot channel of the NORFLOD case compared to the base case are shown in Figure 4.76. In general, the calculated void fraction without using reflood model is a little higher than that of calculation with reflood model. In Figure 4.77, calculated cladding temperatures at various axial elevations of the NORFLOD case are shown. It is seen that high cladding temperatures are sustained for the rest of the reflood period without significant precursory cooling before guench because lower heat fluxes are calculated for the NORFLOD case in the comparison to the base case (see Figure 4.78). Discontinuity of the heat flux calculation is exhibited in the base case at the moment of the reflood model actuation. The calculated vapor temperature comparison shown in Figure 4.79 indicates also a significant vapor temperature increase with the heat transfer package switching. These discontinuities should be further studied to see whether they are real situations.

The comparisons of the cladding temperatures are shown in Figures 4.80, 4.81, and 4.82 for various axial elevations. Significant improvement in the cladding temperature prediction at the hottest section results in the NORFL 3 case study. In Figure 4.80, it is seen that not only the cladding temperatures before quench but also the fuel rod quench temperature and its timing calculated without the reflood model are in good agreement with the test data. These results may indicate that either the criteria used in RELAP5/MOD2 for the actuation of the reflood model calculation are inadequate or the heat transfer package in the reflood model is improper. However, the suggestion of not using reflood model in the L2-5 simulation can not be justified because the accuracy of the RELAP5/MOD2 model in predicting local hydraulic conditions (quality, droplet size, interfacial area, and two phase velocities' is still an open guestion. It would be almost impossible to evaluate separately the heat transfer correlations and hydraulic models in calculating the cladding temperature response during post-dryout dispersed flow conditions.

5. RUN STATISTICS

The computational efficiency of the RELAP5/MOD2 simulations are summarized in Table 5.1. The simulations are conducted on a FACOM M200 computer which is compatible to an IBM MVS system.

6. CONCLUSIONS

In this study, the large break LOCA test L2-5 is analyzed by the RELAP5/MOD2 model. The test simulations begin with break initiation and subsequent blowdown, and continue through lower plenum refill, core reflood, and terminate with corewide quench. Major events and their timings of the lorge break test L2-5 are well predicted by the RELAP5/MOD2 model. Important parameters, such as pressure, break flow, and cladding temperature, are calculated with reasonable agreement in the comparison to the test data. Especially, the most critical parameter in the large break LOCA, the peak cladding temperature, is very well calculated by the RELAP5/MOD2 model. Noticed differences and code deficiencies found in the L2-5 test simulation and various major findings of the sensitivity studies are described in the following:

- 1. The broken loop pressure is well predicted (slightly underestimated) while the pressurizer pressure is significantly underpredicted. The underprediction of the pressurizer pressure is caused by the overprediction of the outsurge flow during blowdown.
- 2. Significant differences in the water level responses between the downcomer near the intact loop and the downcomer near the broken loop are calculated. It indicates that the downcomer modeling employed in this study is quite important in a large break LOCA analysis.

- 3. The effect of the excessive accumulator injection after 50.0 s found in the base case calculation 1. insignificant in determining the transient behaviors of the L2-5 simulation. Since L2-5 failed to measure the accumulator flow rate, the calculated result according to the accumulator model used in the RELAP5/MOD2 calculation (in not be verified. However, according to the comparison of the major event timing, the calculated accumulator flow rate could be a close resemblance to the test condition.
- 4. The hot-leg break flow is overpredicted by RELAP5/MOD2 during early stages of the transient. The measured hot-leg break flow rate shows a hump shape response while the calculated break flow monotonically decreases from its initial peak value during the blowdown period. The break flow increase during blowdown observed in L2-5 could be resulted from momentarily accumulation of the bubbles in the U-tube bend and sequentially the occurrence of the "loop clearance" by the liquid push over. These phenomena could be out of the RELAP5/MOD2 calculation capability. In the sensitivity studies, no improvement in the hot-leg break flow is calculated with various input modifications.
- 5. Flow oscillation observed in L2-5 after ECC injection due to direct contact condensation is calculated by RELAP5/MOD2 with smaller oscillation magnitude than the test data. In the comparison of the fluid temperatures in both the cold-leg and

the downcomer regions, it is found that RELAP5/MOD2 underpredicts the fluid temperature during ECC injection period. These differences indicate a possible deficiency in the condensation model of the present RELAP5/MOD2 code.

- 6. During ECC injection, high density fluid is calculated in the broken loop cold-leg. However, the high density liquid in the calculation is provided by the carryover from the downcomer region instead of the ECC bypass. Compared to the measured density, it is found that the carryover is overpredicted with the interfacial drag model of RELAP5/MOD2.
- 7. According to the cladding temperature measurements located at various axial elevations, the hottest fuel rods from the bottom to the top experience CHF conditions during L2-5 test. The RELAP5/MOD2 calculation, however, shows that only the middle high power portions of the fuel rods suffer from dryout while the lower and upper elevations of the fuel rods stay cooled in the transient analysis. In the sensitivity study with the reduction of the Biasi CHF by a factor of 0.6, the calculation results do not give better predictions of the cladding temperatures at the low power elevations. Moreover, the calculated cladding temperatures at the high power elevations significantly deviate from the test data with the reduction of the CHF.
- With the reflood model calculation, excessive precursor cooling of the fuel rod results which leads to the underesti-

mation of the cladding temperature during the reflood period. Calculation without using the reflood model, not only the calculated cladding temperatures but also the quench temperature and its timing are in very good agreements with the test data. However, the exciting results of this special calculation could be caused by wrong reasons, because the accuracy of the RELAP5/MOD2 model in predicting local hydraulic conditions is still an open guestion. However, the results may indicate that either the criteria used in RELAP5/MOD2 for the actuation of the reflood model calculation are inadequate or the heat transfer package in the reflood model is improper. In any case, the discontinuities of the calculated rod surface heat flux and vapor temperature indicate a discontinuous heat transfer coefficient before and after the actuation of the reflood model. Further review is required for these discontinuity.

9. In the sensitivity studies of the large break LOCA test L2-5, the calculated PCTs of various cases are obtained during the blowdown period. The calculated PCTs are quite insensitive to different input modifications including (1) adjusted accumulator modeling; (2) initial temperature distributions in the broken loop hot-leg; (3) flow resistances of the broken loop hot-leg; (4) discharge coefficient of the critical flow at the hot-leg break; (5) cross-flow junction used for the linkage between the broken loop and the reactor

vessel. However, significant differences in the PCT calculations are found in the studies of the fuel gap dimension and the CHF correlation.

10. With the assumption of having flywheel connected during pump coastdown, the calculation results show that the present RELAP5/MOD2 model does not yield blowdown guench phenomena.

	Table	3.1	Initial	Condi	tions	of	LOCE	Test	L2-	5
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Parameter	L2-5	RELAP5/MOD2
Power level (MW)	36.0±1.2	36.0
Primary colant system mass flow (kg/s)	192.4±7.8	194.97
Hot-leg pressure (MPa)	14.94 ± 0.06	14.935
Intact loop hot-leg temperature (K)	589.7±1.6	589.71
Intact loop cold-leg temperature (K)	556.6±4.0	556.24
Core AT (K)	33.1 ± 4.3	33.47
Broken loop hot-leg temperature (K)	561.9±4.3	565.44
Broken loop cold-leg temperature (K)	554.3 ± 4.2	554.31
S.G. secondary side pressure (MPa)	5.85 ± 0.06	5.548
S.G. secondary side flow (kg/s)	19.1±0.4	18.86
Pressurizer water level (m)	1.14 ± 0.03	1.14

	Time (s)		
		rime (S)	
Event	L2-5	RELAP5/MOD2	
Experiment initiation	0.0	0.0*	
CHF occurred	0.9	0.3	
Primary coolant pump trip	0.94	0.94*	
Liquid level drops below top of core	3.2#	1.7	
Liquid level drops below bottom of core	5.4#	5.0	
Peak cladding temperature reached	30.0	7.0	
Pressurizer empty	14.0	10.0	
Accumulator flow initiation	16.8	15.7	
End of blowdown	22.0#	21.3	
HPIS flow initiation	23.9	23.9*	
Lower plenum refill	31.0#	30.5	
LPIS flow initiation	37.3	37.3*	
Core reflood	55.0#	54.0	
Final core guench	62.0	57.2	
Transient ended	120.0	90.0	

Table 4.1 Sequence of Events in LOCE Test L2-5

* Boundary conditions

Rough estimate from void measurements in the core region

Table 4.2	Cases Analyzed in the Sensi	tiuity Study
	of the LOCE Test L2-5 Simul	ation

Case	Conditions different from the base case
ACCUM50	Smaller accumulator volume (67% of the base case) and accumulator flow tripped-off at 50.0 s
*BLHL-HT	Initial temperature of 590 K (25 K higher than the base case) is specified in the broken loop hot-leg
BLHL-DC	Discharge coefficient of 0.8 (instead of 1.0 in the base case) is used in the hot-leg break
BCHL-5K	Junction form loss coefficents used in the broken loop hot-leg are five times of the base case
PV-X-BL	Cross-flow junction is used in connecting the broken loop to the pressure vessel
MESH#32	Number of reflood fine mesh intervals increases from 8 to 32
*FUEL-GAP	Nominal fuel gap distance of 0.0953 mm (about twice larger than the base case) is assumed without considering possible fuel swelling effect
PUMP-FW	Pump coastdown with 316.04 kg-m ² inertia (instead of 1.431 kg-m ² in the base case) produced by its flywheel system
CHF*0.6	CHF calculated by the Biasi correlation is reduced by a factor of 0.6
NORFLOD	Calculation without the actuation of the reflood heat transfer model

*Initialization process is performed before transient calculation

Case	Transient Time(s)	CPU(s)	Number of Time Step	Number of Volume Cell	* Performance Number
BASE	90	3277.13	6284	128	4.074
BLHL-HT	60	2301.99	4394	128	4.093
BLHL-DC	60	2280.81	4335	128	4.110
BLHL-5K	90	2761.04	5220	128	4.132
PV-X-BL	60	2310.41	4436	128	4.069
MESH#32	60 ;	2423.19	4494	128	4.213
FUEL-GAP	80	2969.44	5825	128	3.983
PUMP-FW	60	2330.01	4452	128	4.089
CHF*0,6	90	3068.71	5992	128	4.001
NORFLOD	80	2685.07	5503	128	3.812

Table 5.1 Run Statistics of the LOCE Test L2-5 Simulation

*Performance Number=

CPU x 10^3 [Number of Time Step] / [Number of Volume Cell]



Figure 1.1 LOFT Facility Major Components





000 000 ¥ 200-00-1 200-200-RELAP5/MOD2-LOFT Large Break Model Nodalization for Experiment L2-5 Broken leop cold leg (33)-(30)-(34) 011 _____ 506 __ 00r] Broken loop hot leg L []]] 1 2 2 2 Reactor vessel I Car 282 256 290 7.87 In-273 201-1 235 1 1111 136 an an 202 202 278 220 230 2.25 322 155 240 215 234 nr-2 23 206 802 052 104 Intact 'oop hot leg 810 - CHIS ã. SUITZEY 019 631 830 55 EDC system 199 110 1011 1000 \$20 1517 1 Figure 3.1 Steam generator Intact loop cold leg 155 515 6 00 158 1 000-525 045 555 -343 2005 1225



Figure 4.1 Comparison between the Calculated and Measured Broken Loop Cold-Leg Pressures of Test L2-5



Figure 4.2 Comparison between the Calculated and Measured Pressurizer Pressures of Test L2-5.



Figure 4.3 Comparison between the Calculated and Measured Pressurizer Water Levels of Test L2-5



Simulation



Figure 4.5 Calculated ECC Flow Rates of Test L2-5 Simulation


Figure 4.6 Comparison between the Calculated and Measured Cold-Leg Break Flow Rates of Test 1.2-5



Figure 4.7 Comparison between the Calculated and Measured Hot-Leg Break Flow Rates of Test L2-5



Calculated Void Fractions Upstream the Break Junctions of Test L2-5 Simulation



Figure 4.9 Comparison between the Calculated and Measured Intact Loop Cold-Leg Flow Rates of Test L2-5



Figure 4.10 Comparison between the Calculated and Measured Intact Loop Hot-Leg Flow Rates of Test L2-5



Figure 4.11 Comparison between the Calculated and Measure 1 Intact Loop Hot-Leg Flow Rates During the Blowdown Period of Test L2-5



Figure 4.12 Calculated Core Flow Rates During the Blowdown Period of Test L2-5 Simulation





Figure 4.14 Calculated Cladding Temperatures at Hot Channel Hot Rod of Test L2-5 Simulation



Figure 4.15 Comparison between the Calculated and Measured Cladding Temperatures of Test L2-5



Figure 4.16 Comparison between the Calculated and Measured Upper Plenum Fluid Temperatures of Test L2-5



Figure 4.17 Comparison between the Calculated and Measured Intact Loop Hot-Leg Fluid Temperatures of Test L2-5



Figure 4.16 Comparison between the Calculated and Measured Broken Loop Hot-Leg Fluid Temperatures of Test L2-5



Comparison between the Calculated and Measured Intact Loop Cold-Leg Fluid Temperatures of Test L2-5



Calculated Fluid Temperatures in Upper downcomer of Test L2-5 Simulation



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Comparison between the Calculated and Measured Downcomer (0.74 m from RV Bottom) Fluid Temperatures of Test L2-5 Figure 4.24



















Comparison between the Calculated and Measured Broken Loop Cold-Leg Densities of Test L2-5



Figure 4.30 Calculated Flow Rates in Broken Loop Cold-Leg of Test L2-5 Simulation



Figure 4.31 Calculated Flow Rates in Reactor Vessel Near Broken Loop Cold-Leg of Test L2-5 Simulation







Figure 4.33 Comparison between Calculated Water Levels in Core Region of the BASE and ACCUM50 Cases



Figure 4.34 Comparison between Calculated Water Levels in Downcomer Near Intact Loop of the BASE and ACCUM50 Cases



Figure 4.35 Comparison between Calculated Water Levels in Downcomer Near Broken Loop of the BASE and ACCUM50 Cases



Figure 4.36 Comparison between Calculated Cold-Leg Break Flow Rates of the BASE and ACCUM50 Cases







Figure 4.38 Comparison between Calculated Cladding Temperatures at Various Axial Locations of the BASE and ACCUM50 Cases



Figure 4.39 Comparison between Calculated Cladding Temperatures at Hottest Location of the BASE and ACCUM50 Cases



Figure 4.40 Comparison between Calculated Hot-Leg Break Flow Rates of the BASE and BLHL-HT Cases



Figure 4.41 Comparison between Calculated Cold-Leg Break Flow Rates of the BASE and BLHL-HT Cases






Comparison between Calculated Cladding Temperatures at Hottest Location of the BASE and BLHL-HT Cases



Figure 4.44 Comparison between Calculated Hot-Leg Break Flow Rates of the BASE and BLHL-DC Cases



Figure 4.45 Comparison between Calculated Broken Loop Cold-Leg Pressures of the BASE and BLHL-DC Cases







Figure 4.47 Comparison between Calculated Cladding Temperatures at Various Axial Locations of the BASE and BLHL-DC Cases



Comparison between Calculated Cladding Temperatures at Hottest Location of the BASE and BLHL-DC Cases Figure 4.48



Figure 4.49 Comparison between Calculated Broken Loop Cold-Leg Pressures of the BASE and BLHL-5K Cases







Figure 4.51 Comparison between Calculated Hot-Leg Break Flow Rates of the BASE and BLHL-5K Cases



Figure 4.52 Comparison between Calculated Cold-Leg Break Flow Rates of the BASE and BLHL-5K Cases



Figure 4.53 Comparison between Calculated Cladding Temperatures at Various Axial Locations of the BASE and BLHL-5K Cases



Figure 4.54 Comparison between Calculated Cladding Temperatures at Hottest Location of the BASE and BLHL-5K Cases



Figure 4.55 Comparison between Calculated Hot-Leg Break Flow Fates of the BASE and PV-X-BL Cases

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Figure 4.56 Ccaparison between Calculated Cold-Leg Break Flow Rates of the BASE and PV-X-BL Cases



Figure 4.57 Comparison between Cladding Temperatures at Various Axial Locations of the BASE and PV-X-BL Cases



Figure 4.58 Comparison between Cladding Temperatures at Hottest Location of the BASE and PV-X-BL Cases



Figure 4.59 Comparison between Calculated Hot-Leg Break Flow of the BASE and MESH#32 Cases



Figure 4.60 Comparison between Calculated Cold-Leg Break Flow Rates of the BASE and MESH#32 Cases



Figure 4.61 Comparison between Calculated Cladding Temperatures at Various Axial Locations of the BASE and MESH#32 Cases



Figure 4.62 Comparison between Calculated Cladding Temperatures at Hottest Location of the BASE and MESH#32 Cases



Figure 4.63 Comparison between Calculated Radial Temperature Distributions in Fuel Rod of the BASE and FUEL-GAP Cases



Figure 4.64 Comparison between Calculated Cladding Temperatures at Various Axial Locations of the BASE and FUEL-GAP Cases



Figure 4.65 Comparison between Calculated Cladding Temperatures at Hottest Location of the BASE and FUEL-GAP Cases



Figure 4.66 Comparison between Calcualted Hot-Leg Break Flow Rates of the BASE and FUEL-GAP Cases



Figure 4.67 Comparison between Calculated Cold-Leg Break Flow Rates of the BASE and FUEL-Gap Cases



Comparison between Calculated Intact Loop Cold-Leg Flow Rates of the BASE and PUMP-FW Cases







Figure 4.70 Comparison between Calculated Cladding Temperatures at Hottest Location of the BASE and PUMP-FW Cases







Comparison between Calculated Cold-Leg Break Flow Rates of the BASE and PUMP-FW Cases



Figure 4.73 Comparison between Calculated Cladding Temperatures at Axial Level 3 of the BASE and CHF*0.6 Cases







Figure 4.75 Comparison between Calculated Cladding Temperatures at Axial Level 5 of the BASE and CHF*0.6 Cases



Comparison between Calculated Voids in Core Region of the BASE and NORFLOD Cases










Comparison between Calculated Vapor Temperatures in Core Region of the BASE and NORFLOD Cases Figure 4.79

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Figure 4.81 Comparison between Calculated Cladding Temperatures at Axial Level 4 of the BASE and NORFLOD Cases





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0000332	MFLOWJ	345020000	* DTT-RAKE BLCL
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1051201 ********** * PRESSUR ************************************	5+8318 *********** 12ER CONNE ********** P2RT**SGS	CTIDN TEE	STEAM GEMI STEAM GEMI STEAM GEMI	FRATOR SIDE	00000000000000000000000000000000000000	*************	000
1051201 ********** * PRESSUR ********** 1100000 1100001	5+8318 *********** 12ER CONNE ********** PZRT*SGS	0.0027 0000000000	STEAM GEMI	FRATOR SIDE	00000000000000000000000000000000000000	980990999999 888809989999	000
1051201 *********** * PRESSUR ********** 1100000 1100001	5+8318 ********** 12ER CONNE ********* PZRT*SGS 1 0-0	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	STEAM GEMI STEAM GEMI SESSESSESSES BRANCH	FRATOR SIDE	0.0		000
1051201 *********** * PRESSUR ********** 1100000 1100001 1100101	5 * 8 3 1 8 * * * * * * * * * * * * 1 ZER CONNE * * * * * * * * * * PZRT ** SGS 1 0 * 0 * 0 = 5	0 0.623	STEAM GEMI STEAM GEMI SESSERES BRANCH 0.0303	0.0	0.0		000
1051201 *********** * PRESSUR ********** 1100000 1100001 1100101 1100102	5 * 8318 ********** 12ER CONNE ********* PZRT**SGS 1 0 * 0 4 * 0=5 000	0 0.623 0.0 14.92856	0.0303 00 1.411854	0.0 2.4615E6	0.0 2.1446-6		000
1051201 *********** * PRESSUR ********** 1100000 1100001 1100101 1100102 1100200	5 * 8318 ********** 12ER CONNE ********* PZRT**SGS 1 0 * 0 4 * 0=5 000	0 0.623 0.0 14.928E6	5.0 5.0 5.0 5.0 5.0 5.0 5.0 5.0	0.0 2.4615E6	0.0 2.1446=6	00200	000
1051201 ********** * PRESSUR ********** 1100000 1100001 1100101 1100102 1100200 1100200	5.8318 2288 CONNE 2287 - SGS 1 0.0 4.0-5 000 110010000	0 0.623 0.0 14.92826 0.0	57544 GEMI 555555555 57544 GEMI 555555555 5755555555 5755555555 57555555	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1	00000	000
1051201 ********** * PRESSUR ********** 1100000 1100001 1100101 1100102 1100200 1101101 1101201	5.8318 28888888888 12ER CONNE PZRT-SGS 1 0.0 4.0-5 000 110010000 5.8320	0 0.623 0.0 14.928E6 112000000 5.8242	57544 GEMI 57544 GEMI 555555555 6RANCH 0.0303 00 1.4118E6 0.0 0.0	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1	00000	9 6 9
1051201 ***********************************	5.8318 	0 0.623 0.0 14.928E6 112000000 5.8242	0.0303 00 1.4118E6 0.0 0.0 0.0 0.0	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1	неўварнаача Фёваранаа Фёваранаа С.О ООСОО Фёваранеана	9 9 9 9
1051201 *********** * PRESSUR ********* 1100000 1100001 1100101 1100102 1100200 1101201 *********	5.8318 ********** IZER CONNE ********** PZRT*SGS 1 0.0 4.0=5 000 110010000 5.8320 ************* S PIPING	0 0.623 0.0 14.928E6 112000000 5.8242	0.0303 00 1.4118E6 0.0 0.0 0.0 0.0	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1	 	000
1051201 ***********************************	5.8318 ********** IZER CONNE ********** PZRT*SGS 1 0.0 4.0=5 000 110010000 5.8320 ************************************	0 0.623 0.0 14.928E6 112000000 5.8242	0.0303 00 1.4118E6 0.0 0.0 0.0 0.0 0.0 0.0	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1 0.0 0.1	 	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
1051201 ********** * PRESSUR ********* 1100000 1100101 1100101 1100102 1100200 1101201 ********* * HOT LEG	5 * 8 3 1 8 * * * * * * * * * * * * 1 ZER CONNE * * * * * * * * * * * PZRT * SGS 1 0 * 0 4 * 0 = 5 0 00 1 1 0 0 1 0 0 0 0 5 * 8 3 2 0 * * * * * * * * * * 0 0 0 1 1 0 0 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * 0 * 0 1 0 0 0 1 0 0 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * 0 * 0 1 0 0 0 1 0 0 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * * 0 * 0 1 0 0 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * * * 1 0 0 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * * * 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * * * * 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * * * * * * HDTLEGPP	0 0.623 0.0 14.928E6 112000000 5.8242	0.0303 00 1.4118E6 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1 ********	 	9 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
1051201 ********** * PRESSUR ********* 1100000 1100101 1100102 1100102 1100200 1101201 ********* * HOT LEG ********* 1120000 1120001	5 * 8 3 1 8 * * * * * * * * * * * * 1 ZER CONNE * * * * * * * * * * * PZRT * SGS 1 0 * 0 4 * 0 = 5 0 00 1 0 0 1 0 0 0 0 5 * 8 3 2 0 * * * * * * * * * * 0 0 0 1 0 0 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * 0 * 0 1 0 0 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * 0 * 0 1 0 0 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * 0 * 0 1 0 0 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * * 0 * 0 1 0 0 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * * 1 0 * 0 1 0 0 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * * * * * 0 * 0 1 0 0 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * * * * * * HDTLEGPP 2	0 0.623 0.0 14.928E6 112000000 5.8242	0.0303 00 1.4118E6 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1 *********	 	9 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
1051201 ********** * PRESSUR ********* 1100000 1100101 1100102 1100102 1100200 1101201 ********* * HOT LEG ********* 1120000 1120001 1120101	5 * 8 3 1 8 * * * * * * * * * * * * 1 ZER CONNE * * * * * * * * * * * PZRT * SGS 1 0 * 0 4 * 0 = 5 000 1 0 0 1 0 0 0 0 5 * 8 3 2 0 * * * * * * * * * * 0 * 0 1 0 0 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * 0 * 0 1 0 0 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * 0 * 0 1 0 0 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * 0 * 0 1 0 0 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * * 0 * 0 1 0 0 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * * 0 * 0 1 0 0 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * * * 0 * 0 0 * 0 1 0 0 1 0 0 0 5 * 8 3 2 0 * * * * * * * * * * * * * * HDTLEGPP 2 0 * 0 * 0	2	0.0303 00 1.4118E6 0.0 0.0 1.90 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 2.4615E6 0.1	0.0 2.1446=6 0.1 ********	айаааааааа айааааааааа айаааааааааааа айаааааа	0 0 0 0 0 0 0 0 0 0 0 0 0
1051201 ********** * PRESSUR ********* 1100000 1100101 1100102 1100200 1101201 ********* * HOT LEC ********* 1120000 1120001 1120101 1120201	5.8318 ********** IZER CONNE ********* PZRT*SGS 1 0.0 4.0=5 000 110010000 5.8320 ********* PIPING ********** HDTLEGPP 2 0.0 0.0 0.0	2 1 2 2 2 2 2 1 2 1 2 1 2 1 2 1 2 1 2 1	0.0303 00 1.4118E6 0.0 0.0 1.918E6 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1 0.0 0.1	 	0 0 0 0 0 0 0 0 0 0 0 0 0
1051201 ********** * PRESSUR ********** 1100000 1100101 1100102 1100102 1100200 1101201 ********* * HOT LEG ********* 1120000 1120001 1120101 1120201 1120301	5.8318 ********** IZER CONNE ********** PZRT=SGS 1 0.0 4.0=5 000 110010000 5.8320 ********** PIPING ********** HDTLEGPP 2 0.0 0.0 1.4385	2 1 2 2 2 1 2 1 2 1 1 2 1 1 2 1 1 2 1 1	0.0303 00 1.4118E6 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1 0.0 0.1	 	0 0 0 0 0 0 0 0 0 0 0 0 0
1051201 ********** * PRESSUR ********** 1100000 1100101 1100102 1100102 1100200 1101201 ********* * HOT LEG ********* 1120000 1120001 1120101 1120201 1120301 1120302	5.8318 ********** IZER CONNE ********** PZRT=SGS 1 0.0 4.0=5 000 110010000 5.8320 ********* HDTLEGPP 2 0.0 1.4385 0.708	2 1 2 2 2 1 2 1 2 2 1 2 2 1 2 2 1 2 2 1 2 2 1 2	0.0303 00 1.4118E6 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1 0.0 0.1	 	0 0 0 0 0 0 0 0 0 0 0 0 0
1051201 ********** * PRESSUR ********** 1100000 1100101 1100102 1100102 1100200 1101201 ********* * HOT LEG ********* 1120000 1120001 1120201 1120301 1120302 1120401	5.8318 ********** IZER CONNE ********** PZRT=SGS 1 0.0 4.0=5 000 110010000 5.8320 ********* HDTLEGPP 2 0.0 1.4385 0.708 0.09	2 1 2 1 2 1 2 1 2 1 2 1 2 1 2 1	0.0303 00 1.4118E6 0.0 0.0 1.4118E6 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1 0.0 0.1	 4 4	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
1051201 ********** * PRESSUR ********** 1100000 1100101 1100102 1100102 1100200 1101201 ********* * HOT LEG ********* 1120000 1120001 1120101 1120201 1120301 1120302 1120401 1120402	5.8318 ********** IZER CONNE ********** PZRT=SGS 1 0.0 4.0=5 000 110010000 5.8320 ********** HDTLEGPP 2 0.0 1.4385 0.708 0.09 0.057	2 1 2 2 2 2 2 2 2 2 2 2 2 2 2	57544 GEMI 57544 GEMI 55555566 68ANCH 0.0303 00 1.411856 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1 0.0 0.1	 4 4	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
1051201 ********** * PRESSUR ********** 1100000 1100101 1100102 1100102 1100200 1101201 ********* * HOT LEG ********* 122000 112000 1120001 1120201 1120301 1120302 1120401 1120402 1120501	5.8318 ********** IZER CONNE ********** PZRT=SGS 1 0.0 4.0=5 000 110010000 5.8320 ********** HOTLEGPP 2 0.0 1.4385 0.708 0.09 0.057 0.0	2 1 2 2 2 2 2 2 2 2 2 2 2 2 2	57544 GEMI 57544 GEMI 55555566 68ANCH 0.0303 00 1.411856 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1 0.0 0.1	 4 4	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
1051201 ***********************************	5.8318 ********** IZER CONNE ********** PZRT=SGS 1 0.0 4.0=5 000 110010000 5.8320 ********** HOTLEGPP 2 0.0 1.4385 0.708 0.09 0.057 0.0 0.0	2 1 2 2 2 1 2 2 1 2 2 1 2 2 1 2 2 1 2 2 2 1 2 2 2 2 2 2 2 2 2 2 2 2 2	57544 GEMI 57544 GEMI 55555566 68ANCH 0.0303 00 1.411856 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1 0.0 0.1	 4 4	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
1051201 ***********************************	5.8318 ********** IZER CONNE ********** PZRT=SGS 1 0.0 4.0=5 000 110010000 5.8320 ********** HOTLEGPP 2 0.0 1.4385 0.708 0.09 0.057 0.0 0.0 0.0 0.057 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	2 1 2 2 2 1 2 2 1 2 2 1 2 2 1 2 2 2 2 2 2 2 2 2 2 2 2 2	57544 GEMI 57544 GEMI 55555566 6RANCH 0.0303 00 1.411856 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1 0.0 50555455555555555555555555555555555	аловорана обраново 0.0 0.00 0.00 0.00 0.0000 0.0	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
1051201 ***********************************	5.8318 ********** IZER CONNE ********** PZRT=SGS 1 0.0 4.0=5 000 110010000 5.8320 ********** HOTLEGPP 2 0.0 1.4385 0.708 0.09 0.057 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	2 1 2 2 1 2 2 2 1 2 2 2 2 2 2 2 2 2 2 2 2 2	57544 GEMI 57544 GEMI 55555566 6RANCH 0.0303 00 1.411856 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1 0.0 0.1	20000000000000000000000000000000000000	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
1051201 ***********************************	5.8318 	2 1 2 2 1 2 2 1 2 2 1 2 2 1 2 2 2 2 2 2 2 2 2 2 2 2 2	0.0303 00 1.4118E6 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1 0.0 0.1	20000000000000000000000000000000000000	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
1051201 ***********************************	5.8318 	2 1 2 2 1 2 2 2 2 2 2 2 2 2 2 2 2 2	22 22 22 22 22 22 22 22 22 22 22 22 22	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1 0.0 0.1	20000000000000000000000000000000000000	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
1051201 ***********************************	5.8318 	2 1 2 2 1 2 2 1 2 2 1 2 2 2 1 2 2 2 2 2 2 2 2 2 2 2 2 2	22 22 22 22 22 22 22 22 22 22 22 22 22	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1 0.0 0.1	************ *************************	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
1051201 ***********************************	5.8318 	2 1 2 2 1 2 2 2 1 2 2 2 2 2 2 2 2 2 2 2 2 2	2 2 2 2 2 2 2 1	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1 0.0 0.1	************ *************************	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
1051201 ***********************************	5.8318 	2 1 2 2 1 2 2 1 2 2 2 2 2 2 2 2 2 2 2 2 2	22 22 22 22 22 22 22 22 22 1	0.0 2.4615E6 0.1	0.0 2.1446-6 0.1 0.0 5000000000000000000000000000000	************ *************************	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
1051201 ***********************************	5.8318 	2 1 2 2 1 2 2 1 2 2 2 2 2 2 2 2 2 2 2 2 2	22 22 22 22 22 1 22 22	0.0 2.4615E6 0.1 **********	0.0 2.1446-6 0.1 0.0 0.1 0.0 0.1 0.0 0.1	************* ************************	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
1051201 ***********************************	5.8318 	2 1 2 2 1 2 2 1 2 2 1 2 2 1 2 2 1 2 2 2 1 2 2 2 1 2 2 2 1 2 2 2 1 2 2 2 1 2 2 2 1 2 2 2 1 2 2 2 1 2 2 2 1 2 1 2 2 1 2 2 1 2 2 1 2 2 1 2 2 1 2 2 1 2 2 2 2 1 2 2 2 2 2 2 2 2 2 2 2 2 2	22 1 44115E 22 1 24115E 22 1 22 1 22 1 22 1	6 2.4615E6	0.0 2.1446-6 0.1 0.0 5.5532-	**************************************	0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.0

\$

1121300	0						
1121301	4.5335	4.5325	0.0	01			

* 5G 1NL	ET PLENUM						
*******	80000000000000000000000000000000000000		******	*********			
1160000	SGINPLNM		BRANCH				***
1140001	2	0					
1140101	0.0	0.63	0.335	0.0	90.0	0.513	
1140102	4 . 0 = 5	0.0	00			~ ~ ~ ~ ~	
1140200	000	14.92126	1.4118E6	2.461786	1.7048+3		
1141101	112010000	114000000	0.0512	1.10000	1.10000	00000	
1142101	114010000	115000000	0.0	0.20000	0.20000	00000	
1141201	5.5399	5.5567	0.0				
1142201	1.8785	1.8792	0.0				
***	10444444444	0	66686666666	******	********		000
* 50 U+T	JEES						
84000084	0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.	00000000000000000000000000000000000000	000000000000000000000000000000000000000	800000000			0.54
1150000	SG=TUBES		PIPE				
1150001	8						
1150101	0.151	8					
1150201	0.151	7					
1150301	0.902	1					
1150302	0.6096	3					
1120202	0+4612	2					
1140304	0.0090	1					
1140401	0.902	8					
1150501	0.0	5					
1150601	0.0	0					
1150602	-00.0	~					
1150701	0.000	0					
1150702	0.6096	a a					
1150703	0.3048	4					
1150704	-0.3048	6					
1150705	-0.6096	7					
1150706	-0.902	8					
1150801	1.27-7	0.01022	8				
1150901	0.0	0.0	7				
1151001	00	8					
1151101	00000	7					
1151201	000	14.914E6	1.3694E6	2.4618E6	3.2232-9	0.0	
1151202	000	14.907E6	1.3352E6	2.4620E6	8.1280-10	0.0	3
1151203	000	14.901E6	1.3074E6	2.4621E6	2.0175-10	0.0	3
1151204	003	14.897E6	567.83	0.0	0.0	0.0	6
1151205	003	14.896E6	564.85	0.0	0.0	0.0	5
1151206	003	14.898E6	561.53	0.0	0.0	0.0	6
1151207	003	14.90166	558.68	0.0	0.0	0.0	7
1131208	003	14.905E6	556.21	0.0	0.0	0.0	8
1161301	0	dialog in					
11513001	1.8310	1.8310	0.0	01			
1151302	1 7401	1.7401	0.0	02			
1151304	1.7534	1 7696	0.0	03			
1151305	1.7334	1 7304	0.0	04			
1151306	1.7340	1 7240	0.0	05			
1151307	1.7128	1.7120	0.0	00			
*****		401420 60666666	0.00	Q.1			
* SG OUTI	ET PLENUM			a#650655555	196955556666	000000000000000	6.6.9
******	*********	*******					
1160000	SGOTPLAN		BRAUCH	**********	**********	*********	000
1160001	2	0	Sector Contractor				
1160101	0.0	0.63	0.335	0.0	+90.0	+0.513	

A-5

1160102 4.0-5	0.0	00				
1160200 003	14.910EA	556.21				
1161101 115010000	116000000	0.0	0.20000	0.20000	00000	
1162101 116010000	118000000	0.0512	1.10000	1.10000	00000	
1161201 1.7026	1.7026	0.0				
1162201 5.0213	5.0213	0.0				
***************	*******		*****	000000000000	******	4
* PUMP SUCTION PIPIN	1G					
*****	0 * * * * * * * * * * * * * * * * * * *	100日日日日日日日日日日日日日日日日日日日日日日日日日日日日日日日日日日日	****	******	****	\$
1180000 PMPSUCPP		PIPE				
1180001 3						
1180101 0.0	2					
1190102 0.0634	3					
1180201 0.0	2					
1180301 0.547	1					
1180302 0.689	2					
1180303 0.559	3					
1180401 0.0437	1					
1180402 0.0462	2					
1180403 0.0	2					
1180501 0.0	2					
1180501 =90.	2					
1180701 -0.498	*					
1150702 =0.687	6					
1150703	20					
1100001 4:0-2	0.083	1				
1100701 0:000	0-104	5				
1181001 00	3	*				
1181101 00000	2					
1181201 003	14.900F6	556.21	0.0	0.0	0.0 1	
1181202 003	14.90266	556.21	0.0	0.0	0.0 2	
1181203 003	14.904E6	556.21	0.0	0.0	0.0 3	
1181300 0						
1181301 3.8342	3.8342	0.0	01			
1181302 4.0551	4.0551	0.0	02			
教育教育教育教育教育教育教育教育教育教育	1.2.2.4.4.4.4.4.4.4.4.4.4.4.4.4.4.4.4.4.	00000000000000000000000000000000000000	****	000000000000	000000000000000	ġ.
· PUMP SUCTION TEE			la de la composition de comp			
99000000000000000000000000000000000000	○ 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	0.00 A U #U	**********	*********	*****	N.
1200000 PMPSUCTE		DRAGCH				
1200001 3	0.74	0.0	0.0	0.0	6.6	
1200101 0.0534	0.10	0.0	14 A V	0.0	×**	
1200102 4:0-2	14.90456	556.21				
1201101 110010000	120000000	0.0	0.20000	0.200000	00000	
1202101 120010000	125000000	0.0	0.5	0.5	00000	
1203101 120010000	155000000	0.0	0.5	0.5	00000	
1201201 4.0551	4.0551	0.0				
1202201 2.1013	2.1013	0.0				
1203201 2.1053	2.1053	0.0				
***	*****	0444444444	******	*********	*****	Q.
* PUMP 1 SUCTION TEL	E DUTLET				and also in the set	
***	******	****	****	*****	*****	8
1250000 PMPSUCTE		BRANCH				
1250001 1	0			0.0.0	0.501	
1250101 0.0	1.003	0.0613	0.0	40.0	0.1257	
1250102 4.0+5	0.0	00				
1250200 003	14.906E6	556.21	0.0	0.0	00000	
1251101 125010000	130000000	0.0	0.0	V.V.	00000	
1251201 3.1053	3.1033	0.0	*********		******	45
S DIND 1 IN FT	*********	****	*********			

				****	******	
1300000	PUPINET		SNRLVOL	**********		00000000000000000
1300101	0.0	0.457	0.0189	0.0	90.0	A 187
1300102	4.0-5	0.0	00	V * V	VU.V.V	A * 1. 3 1
1300200	003	14.9COF6	556.21			
*****		*******	848888888888		******	*********
* PRIMARY	COOLANT PI	UMP 1				*****
********	*******			*********		
1350000	PCPU4P1		PUMP			
1350101	0.0366	0.0	0.039	0.0	90.0	0.319
1350103	0					
1350108	130010000	0.0	0.1	0.1	00000	
1350109	140000000	0.0	0.1	0.1	00000	
1250200	003	14.93486	556.23			
1350201	0	3.5027	3.5089	0.0		
1350202	0	3.5088	2,5088	0.0		
1000001	0 0	0	-1	-1	516	0
100002	369.7	0:3341	0.3155	96.0	500.6	1.431
1350303	613.6	0.0	207.433	0.0444	19.5987	0.0
1330310	0+0	0.0	0*0			
4 DI14D 1		N A100		*****	你你你你你你你你	*****
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1400000	DHDILITI T		\$1.00 × 0 × 0 × 0 × 0 × 0 × 0 × 0 × 0 × 0	*********	00000000000	DDDDDDDDDDDDDDDDDDDDDDDD
1400101	0.0366	6.665	SHOLVUL	A A		
1400102	4.0-5	0.0	V.V	0.0	0.0	0.0
1400200	003	16.07164	556 54			
	000 000 000	47471450	220:64			********
. PUMP 1	UTLET PIP	E TEE SLO		*******	*********	*********
********		66666666666			******	
1450000	PMPIOUT		BRANCH			***********
1450001	2	0	Specific angel C			
1450101	0.0	1.4084	0.0633	0.0	0.0	0.0
1450102	4.0-5	0.0	00			~ • * *
1450200	003	14.97226	556.24			
1451101	140010000	145000000	0.0	0.0	0.0	00000
1452101	145010000	150000000	0.0366	0.40000	0.40000	00000
1451201	3.5086	3.5086	0.0			
1452201	3.5086	3.5036	0.0			
****	*********	*********	********	****	******	*******
· PUMP OUL	ET TEE					
85686886644 8568686644	·***	00000000000000000	(你你你你你你你你你。	**********	0004444444	*****
1500000	PMPOUT*T		BRANCH			
1500001	2	0				
1500101	0.0634	0.4966	0.0	0.0	0.0	0.0
1500202	4+0=2	0.0	00			
1501101	170010000	14:70/20	226.24		a saint	
1502101	170010000	1750000000	0.0366	0.40000	0.40000	00000
1501201	3.5154	3 5154	0.0	0.0	0.0	00000
1502201	D= 2124	2 . JIJ4	0.0			
******	**\/J***	**************************************	U.S.V.	enniere.		and a state of the second
# PUMP 2	SUCTION TE	E OUTLET	*********	********	**********	0.5.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0
*********		********				
1550000	PUMP2SCT		BRANCH			***********
1550001	1	0				
1550101	0.0	1.003	0.0613	0.0	90.0	0.521
1550102	4.0-5	0.0	00			
1550200	003	14.906E6	556.21			
1551101	155010000	160000000	0.0	0.0	0.0	00000
1551201	3.1112	3.1112	0.0			
******	********	800000000000		**********		

# PUMP 2	INLET PIP	F				
	555555555555555555555555555555555555555					
1600000	PHP2INLT		CK CL VIDI	*********	*********	0.0000000000000000000000000000000000000
1600101	0.0	0.457	0.0100			
1600102	4.0-5	0.0	0.0103	8+9	90.0	0.457
1600200	003	14.90056	556 95			
		2474 PVUCD	220424		1710-1 e H	
* PRIMARY	COOLANT P	UNP 2		06.0000001	0000000000000	· 查到最新的保持的资源的资格
	4555555555	0000000000				
1650000	PCPUHP2		Dividio	**********	1902593999555	1.1.1.1.1.1.1.1.1.1.1.1.1.1.1.1.1.1.1.
1650101	0.0366	0.0	0.000	A		the set of the
1650102	0	V.8.V	2.442.3	0.0	43.0	0.319
1650108	160010000	0.0	0.4	1 ST2		
1650109	170000000	0.0	0.1	0.1	00000	
1650200	003	14.93454	556.03	V+4	00000	
1650201	0	3.5156	3.6186	A		
1650202	õ	3.5165	3.5165	U.U.		
1650301	136 135	135	217427	5 4 V		
1650302	369.7	0.3541	0.3168	01 0	210	· · · · · · · · · · · · · · · · · · ·
1650303	613.6	0.0	307 433	90 + U	200.0	1.431
1650310	0.0	0.0	0.0	C/ g () to be re	71.13401	0.40
********		UBEBEBEELSI	LESSBORE			
# PUMP 2	OUTLET				*********	0000000000000000000
	*********				*********	*********
1700000	PNP2OUTT		BRANCH	esecan cen		0000000000000000
1700001	0	Ö	with the			
1700101	0.0366	0.514	0.0	0.0	0.0	
1700102	4.0=5	0.0	00	V # V	V.V	0.0
1700200	003	14.97166	556.00			
*********	**********		000000			
# INTACT	LOOP COLD	LEG PIPE		**********		***********
******	********					
1750000	ILCLP1	BRANCH				***************
1750001	1	0				
1750101	0.0634	0.559	0.0	0.0	0.0	6.6
1750102	4.0+5	0.0	00	V.V	v.v	N
1750200	003	14.967E6	556.24			
1751101	175010000	176000000	0.0	0.0	0.0	00000
1751201	4.0549	4.0549	0.0		***	00000
6						
1760000	ILCLP2	BRANCH				
1760001	0	0				
1760101	0.0634	0.613	0.0	0.0	0.0	0.0
1760102	4 . 0 - 5	0.0	00			N 8 5
1760200	003	14.96726	556.24			
******	*****	******	****			
* ECC CONT	VECTION TEE					
***	*****	*******				
1800000	ECC=T		BRANCH			
1800001	1	0				
1800101	0.0634	1.152	0.0	0.0	0.0	0.0
1800102	4.0=5	0.0	00			
1800200	003	14.965E6	556.24			
1801101	176010000	180000000	0.0	0.20700	0.20700	00000
1801201	4:0549	4.0549	0.0			
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* REACTOR	VESSEL NO	ZZLE-INTA	CT LOOP C	OLD LEG		
*******	*********	*******	00000000000000	*********	0.0000000000000000000000000000000000000	0000000000000000
1050000	RVN-ILCL		BPATICH			
1050001	2	0				
1850101	0.0634	1.01	0.0	0.0	0.0	0.0
1020102	A. 0=5	0.0	00			

1850200 1851101 1852101 1851201 1852201	003 185010000 180010000 4.0549 4.0549	14.964E6 202000000 185000000 4.0549 4.0549	556.24 0.0634 0.0 0.0 0.0 0.0	1.43960 0.20700	0.80400	00000	,0000
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2000101	6.0	1					
2000301	0.33	î					
2000401	0.0428	1					
2000501	0.0	1					
2000601	90.0	1					
2000701	0.33	7					
2000801	3.81-6	0.178	1				
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2001201	003	10*20050	225.22	U.O.	O.O.	U.S.C.	inens
& UNCTIO	N RETUEEN	UDDED INI	ET AUNTING	AND RI	ATTOM VOLU	48888888888 48 1	0 * 5 0 *
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2010000	1200-202		SNGLJUN				
2010101	200000000	202000000	0.0	0.0	0.0	001.00	
2010201	0	-0.15613	-0.15613	0.0			
********	********	*********	*********		*****	*****	00000
* INLET	ANNULUS	BOTTOM V	OLUME 1				
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2020000	INANBOT1		ANNULUS				
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2020001 2020101 2020301 2020401 2020501 2020601 2020801 2021201 2021201 2021201 2021201 2021201 2030201 2030201 2030201 2030201 2030201 2030201 2030201 2040000 2040001 2040001 2040001 2040501 2040601	1 0.0 0.424 0.055 0.0 -90.0 -0.424 3.81-6 00 003 003 003 003 003 003 003	1 1 1 1 1 1 1 1 1 1 1 1 1 1	1 555.24 0.05 BUTTO 0.0 BUTTO 0.0 3.0332 0.0332 0.00 3.0332 0.00 0.0 3.0332	0.0 \$0000000000000000000000000000000000	0.0 0.0 0.0 0.204 0	0.0 8000000 CDNER 1 8000000 80000000	
2020001 2020101 2020301 2020301 2020501 2020501 2020601 2021001 2021201 2021201 2021201 2021201 2030201 2030201 2030201 2030201 2030201 2030201 2030201 2040000 2040001 2040001 2040501 2040601 2040701	1 0.0 0.424 0.055 0.0 -90.0 -0.424 3.81-6 00 003 003 003 003 003 003 003	1 1 1 1 1 1 1 1 1 1 1 1 1 1	1 555.24 040000000000000000000000000000000000	0.0 \$000000000 11 VOLUME 1 0.22632 0.0 \$0.0	0.0 0.0 0.0 0.204 0	0.0 888888888 COMER 1 880888888 00000 8888888888	

2041001 00 003 2041201 14.96366 556.24 0.0 0.0 0.0 - 1 25 * JUNCTION BETWEEN DRWNCOWER 1.1 AND 1.2 2050000 SNGLJUN J1.1-1.2 2050101 204010000 206000000 0.0 0.0 0.0 00000 2050201 0.1 0 2.9165 2.9165 * DOWNCOMER 1.2 2060000 DWNCR1.2 ANNULUS 2060001 1. 2060101 0.071 1 2060301 0.958 1 2060401 0.0 1 2060501 0.0 1 2060601 -90.0 1 2060701 -0.958 3 2060801 3-81-6 0.1.02 1 2061001 00 2061201 003 14.97CE6 556.24 0.0 0.0 0.0 1 65 * JUNCTION BETWEEN DOWNCOMER 1.2 AND 1.3 4 2070000 J1.2 1.3 SNGLJUN 2070101 206010000 208000000 0.0 0.0 0.0 00000 2070201 2.8162 2.8152 0 0.0 - 25 * DOWNCOMER 1.3 -6 2080000 DWNCR1.3 ANNULUS 2080001 1 2080101 0.071 1 2080301 0.958 1 2080401 0.0 1 2080501 0.0 1 2080601 -90.0 1 2080701 -0.958 2080801 3-81-6 0.102 1 2081001 00 2081201 003 14.977E6 556.23 0.0 0.0 0.0 1 * JUNCTION BETWEEN DOWNCOMER 1.3 AND 1.4 2090000 J1.3-1.4 SNGL JUN 2090101 208010000 210000000 0.0 0.0 0.0 00000 2090201 2.7403 2.7403 0 0.0 * DOWNCOMER 1.4 2100000 DWNCR1.4 ANNULUS 2100001 1 2100101 0.071 1 2100301 0.958 1 2100401 0.0 1 2100501 0.0 1 2100601 -90.0 1 2100701 -0.958 1 2100801 3.81=6 0.102 1 2101001 00 2101201 003 14.98486 556.23 0.0 0.0 0.0 1

*********	*********						688
. LOWER PL	ENUM TOP V	OLUME					
******	查卡 资料资料 计存在 计存在	0000000000000000	1.公布最存在外的有有		********		000
2150000	LWRPLTOP		BRANCH				
2150001	£.	0					
2150101	0.740	0.360	0.0	0.0	+90.	-0.360	
2150102	3.81=6	0.0	00				
2150200	003	14.98926	5523				
2151101	210010000	215000000	0.0	0.72650	0.17160	00000	
2152101	215010000	220000000	0.0	0.0	0.0	00000	
2153101	215000000	225000000	0.15	1.40372	1,14100	00000	
2154101	290010000	215000000	0.0	0.72650	0.17160	00000	
2151201	2.9689	2.9689	0.0				
2152201	2.7292+6	2.7292-6	0.0				
2153201	1.7138	1.7138	0.0				
2154201	0.65179	0.65179	0.0				
********	****						
* LOWR PLE	NUM BOTTO	4 VOLUME					
********	******			*******		ABBRENERLE	
2200000	LWRPLBDT		SNGLVOL				
2200101	0.790	0.370	0.0	0.0	- 90.	-0.370	
2200102	3.81-6	0.0	00	M . W		-0.210	
2200200	003	14,99256	559.38				
*******	*******						
* LOWER CO	RE SUPPORT	T STRUCTUR				*********	
******	0.0000000000			*****		*****	
2250000	LCORESUP		BRANCH		**********	*****	1568
2250001	3	0					
2250101	0.25	0.52	0.0	0.0	0.0	0.60	
2250102	3-81-6	0.095	00	V.V.	30.	0.22	
2250200	003	14.98456	556.33				
2251101	225010000	226000000	0.0	1 46064	1 42041		
2252101	225010000	227000000	8.23260-5	0.60903	0.71330	00000	
2253101	225010000	233000000	1.53281-3	0.60015	0 75400	00000	
2251201	0.66670	0.66670	0.6	0.01012	0.12440	00000	
2252201	2.5488	2.5488	0.0				
2253201	2.4289	2.7226	0.0				
******		000000000000	0.00000000000			enunia	
* CORE BYP	ASS VOLUM	F		**********		00000000000	0000
*******		-		*****			
2260000	CORFRYPS		PIPE	********	**********	*********	0000
2260001	3		1 4 F W				
2260101	0.015	5					
2260201	0.0	2					
2260301	0.559	5					
2260302	0-657	3					
2260401	0.0	4					
2260501	0.0	3					
2260601	0.0	4					
2260801	4-0-5	0.003					
2260901	4.042	0.000					
2261001	0.0	3	<i>£</i>				
2261101	00000	0					
2261201	00000	16 07077	664 00				
2261201	000	14 072ED	220.22	0.0	0,0	0.0	1
2261202	003	14.71320	220+23	0.0	0.0	C*0	2
2241300	003	74* 30150	220.53	0.*0	0.0	0.0	3
2261300	0 41471	5 442 B.	0.0				
2261301	0.00011	0.000/1	0.0	01			
8 CC 1 3 0 K	0.00011	0*00011	0.0	02			
**********	80000000000000000000000000000000000000	********	***	199999999999999	00000000000000000000000000000000000000	1	****

ACTIVE CURE

å

000000000 0	**********		000000000000000000000000000000000000000		00000000000	**********
*****	CURE AVER	NGE CHANNEL	(227/228	,229,230,2	31,232)	
* BRANCH	(227)					
2270000	AVCORE1	BRANCH				
2270101	0.138436	0.27950	0.0	0.0	90.0	
2271101 2272101 2271201 2272201	227010000 233000000 1.7456 -3.1096-3	220000000 227000000 1.8880 +3.4875-3	0.121430 0.239275 0.0 0.0	0.05320 4.69	0.03320 4.69	00000
. BRANCH	(228)					
2280000 2280001 2280101	AVCORE2 2 0.138435	BRANCH 0 0.27950	0.0	0.0	90.0	
2280102	0.27950	1.27-7	0.012	00	6 7400-6	
2281200 2282101 2282201 2282201	228010000 234000000 1.7869 5.5703=4	229000000 228000000 1.9737 8.2698-4	0.121430 0.239275 0.0 0.0	2.400520 0.05320 4.69	0.05320	00000 00703
* BRANCH	(229)					
*	AND OF A	COMMEN.				
2290001	2	0				
2290101 2290102 2290200 2291101 2292101 2291201 2292201	0.138436 0.27950 000 229010000 23500000 1.8079 -1.3281-2	0.27950 1.27-7 14.974E6 230000000 229000000 2.0028 -2.7326-2	0.0 0.012 1.3467E6 0.121430 0.239275 0.0 0.0	0.0 00 2.460586 0.05320 4.69	90+0 3.0013~3 0.05320 4.69	00000
. BRANCH	(230)					
2300000	AVCORE4	BRANCH				
2300101	0.1384.36	0.279.0	0.0	0.0	90+0	
2300102 2301101 2302101 23012°* 23022	0.27950 000 230010000 236000000 1.8661 1.1899-2	1.2747 14.971E6 231000000 230000000 2.0884 1.8866+2	1.3817E6 0.121430 0.239275 0.0 0.0	2.4605E6 0.05320 4.69	3.2853-3 0.05320 4.69	00000
. BRANCH	(231)					
2310000	AVCORES	BRANCH				
2310101 2310102	0.138436 0.27950	0.27950 1.27-7	0.0	0.0	90.0	
2310200 2311101 2312101	000 231010000 237000000	14.969E6 232000000 231000000	1.4010E6 0.121430 0.239275	2.4606E6 0.05320 4.69	1.3774=3 0.05320 4.69	00000

2312201 -2.2904-2 -5.1744-2 0.0 * BRANCH (232) 4 2320000 AVCORE6 BRANCH 2320001 2 0 2320101 0.138436 0.37750 0.0 0.0 90.0 2320102 0.37750 1.27-7 0.012 00 2320200 000 14.96656 1.409366 2:460766 1.4438=3 2321101 232010000 240000000 9.78055-2 0.887340 0.887200 2322101 238000000 232000000 0.239275 4.69 4.69 2321201 2.4159 2.5666 0.0 2322201 5.2195-2 8.2698-2 0.0 4 ***** CORE HOT CHANNEL (233,234,235,236,237,238) . * ERANCH (233) 2330000 HTCORE1 **BPANCH** 2330001 2330101 2.10439-2 0.27950 0.0 0.0 90.0 2330102 0.17950 1.27-7 0.012 00 2330200 000 14.97926 1.274466 2.460466 3.5939-5 233010000 234000000 2.21109-2 0.04981 0.04981 2331101 2331201 1.7548 1.9930 0.0 # BRANCH (234) 2340000 HTCORE2 BRANCH 2340001 12.1 O 2340101 2.50439-2 0.27950 0.0 0.0 90.0 2340102 1.27-7 0.27950 0.012 00 2340200 14.976E6 000 1.339986 2.460586 1.7943-2 2341101 234010000 235000000 2.21109-2 0.04981 0.04981 00000 2341201 1.8382 2.0253 0.0 44 # BRANCH (235) * 2350000 HTCORE3 BRANCH 2350001 2350101 2.50439-2 0.27950 0.0 0.0 90.0 2350102 0.27950 1.27-7 0.012 00 2050200 000 14.974E6 1.398586 2.460586 4.9742-2 2351101 235010000 236000000 2.21109-2 0.04981 0.04981 00000 2351201 2.1092 2.3011 0.0 * BRANCH (236) 45 2360000 HTCORE4 BRANCH 2360001 Ö 2360101 2.62243-2 0.27950 0.0 0.0 90.0 236010* 1.27-7 0.27950 0.012 00 2360200 000 14.97166 1.440166 2.460666 6.8761-2 236010000 237000000 2.21109-2 0.04981 2361101 0.04981 00000 2361201 2.0708 2.4552 0.0 45 . BRANCH (237) 10 2370000 HTCORE5 BRANCH 2370001 0 1 2370101 2.50439-2 0.27950 0.0 0.0 90:0 2370102 0.27950 0.012 1.27-7

2370200 14.969E6 1.4603E6 2.4606E6 6.00+6=2 2371101 237010000 238000000 2.21109-2 0.04981 0.04981 00000 2371201 2.3519 2.9438 0.0 * BRANCH (238) 2380000 HTCORE6 2380001 2380101 2.62243-2 0.37750 0.0 0.0 90.0 2380102 0.37750 1.07=7 00 0.012 2380200 1.470556 2.460656 000 14.966E6 3.5 ; 238010000 240000000 1.50001-2 0.99580 2381101 0.9457. 00060 2381201 2.5780 4.6181 0.0 15 . UPPER END BOXES AND SUPPORT STRUCTURE ****** 2400000 UPRENDEX -RRANCH 1 2400001 2400101 0.297 0.559 0.0 0.0 90 . 0.559 2400102 00 3.81-6 0.145 2400200 14.96166 000 1.4114E6 2.4608E6 1.5489=3 226010000 240000000 0.0 2401101 2.93767 2.93767 00000 0.66672 0.74886 0.0 2401201 . UPPER CORE SUPPORT STRUCTURE - CRUSS FLOW REGION 2450000 UPRCRSUP ERA', CH 2450001 2 0 2450101 0.297 0.559 0.0 0.0 90. 0.559 2450102 0.145 00 3.81-6 2450200 000 14.958E6 1.411766 2.4609E6 2.8155-4 2451101 240010000 245000000 0.0 0.0 0.0 2452101 245010000 251000000 0.0 0.0 0.0 2451201 0.0 0.95598 1.1248 0.0 2452201 4.5990-6 0.24995 . UPPER FLOW SKIRT REGION 最多数的最终条条件条款的现在分词存在在自动在长期合作在有效有效在有效有效有效的有效有效的和效率有效的有效在在存在的方式在不可以不可以不可以 2500000 UFLWSKRT BRANCH 2500001 1 0.843 0.0 2500101 0.114 0.0 90.0 0.843 2500102 3.81-6 2500200 14.951E6 1.4117E6 000 2.461366 7.1467-5 245010000 25000000 0.0 2501101 0.0 0.0 00000 2501201 2.4884 2.6192 0.0 · DEAD END OF FUEL MODULES SNGLVOL 2510000 DEFLMODS 2510101 0.183 0.700 0.0 90.0 0.700 0.0 2510102 0.214 00 3.81-6 2510200 000 14.95466 1.431366 2.461066 2.6921-2 * COMBINED UPPER PLENUM BOTTOM VOLUME 物物酶植物物酶物物物物物物物物物,这些产品的存在的有品种的存在在自己的存在中心的存在分词在在中心在在自己的分词的分子分子分子。 2550000 UPRPLBOT BRADCH 2550001 0 1 2550101 0.0 0.268 1.566 0.0 90.0 1.536 00 2550102 0.0 3.81-6 2550200 000 14.945E6 1.4156E6 2.4612E6 1.7143-3 0.006 2551101 250010000 255000000 0.0 0.006 00000

你会对任你的职作的	教教教教教教教教教教	特尔特特雷尔斯特拉尔	******				4.45
2820000	INAN80T2		ANNULUS				
2820001	1						
2820101	0.0	1					
2820301	0.424	1					
2820401	0.0550	4					
5490505	0.0000 5.6	*					
0000201	0.0	1					
2020001	-40+0 ·	1					
2820701	-0,424	5					
2820801	3.81=6	0.172	1				
2921001	00	1					
2821201	003	14.95886	556.25	0.0	0.0	0.0	41.1
**********	*********	8888888888	******			Ver	*
# JUNCTION	BRTUERN 1	HERT ANNUL	US DOTTOU	VPI INT A	1 11A AT	19999999999999999 1899 - 6	0.41
560086888ND	KARAAAAAAA	NAMES DISCUS	VE DUITIN	ANTONE K 1	PLAD DIAMORE DI	ER 2	
5840000	1525.421		0088559555	0000000000000	04040000000	*********	5.4
2031/202	75255-564		SNGLJUM				
2030101	\$95010000	284000000	0+0	0.22632	0.20490	00000	
2630201	0	0.58777	0.58777	0.0			
활자증진화산전 환신	********	*******	资料得过最佳的存益				6.5
* DOWNCOME	R 2						
******	*******						
							19.6
* DOWNCOMP	R 2.1						
5	10 A 8 4						
2840000	NUMPER A		and states a state				
6040000 0010000	BustedS*T		ANNULUS				
2040001	1						
2840101	0.071	1					
2840301	0.958	1					
2840401	0.0	1					
2840501	0.0	1					
2840601	-90.0	7					
2040001	-20.0	1					
2040721	-0.908	1					
2840801	3.81-6	0.102	1				
2841001	00	1					
2841201	003	14.963E6	556.24	0.0	0.0	0.0	
*				~ * * *	~ * * *	V	*
. JUNCTION	BETWEEEN	DOWNCOWER	2.1 41 6	0.0			
4	C. S. M. C. C. M. M. M. S.	Security of the	ear we b	6.06			
2850000	12 1 - 5 5		error and				
2000000	JGel=ZeZ		SHOLJUN				
CODULUI	284010000	286000000	0.0	0.0	0.0	00000	
2850201	0	0.70438	0.70438	0.0			
* DOWNCOME	R 2.2						
8							
2860000	DWNCR2.2		ANNUL US				
2860001	1		WUMMERS.				
5040101	A 074						
2000101	0.011	1					
2860301	0.958	1					
2860401	0.0	1					
2860501	0.0	1					
2860601	-90.0	1					
2860701	-0.050	4					
2000101	-0.920						
2000001	3+81=6	0+105	1				
5461001	00	1					
2861201	003	14.97026	556.23	0.0	0.0	0.0	
*						w . v	4
* JUNCTIO	1 BETWEEFN	DOWNCOMER	2.2 AND	2.3			
8	and the second second	and showing					
2870000	12.2.2.3		Shids and				
2870101	282010000		511062011			and the second second	
2070201	200010000	200000000	0.0	0.0	0.0	00000	
202010201	0	0.80453	0.80458	0.0			

P

2551201 1.0411=6 0.17006 0.0 * CROSSFLOW JUNCTION BETWORN UPPER INLET ANNULUS 1 AND 2 2700000 UINCR-FL SNGLUUN 2700101 200010000 280010000 5.86740-2 98.0000 18.0000 2700201 0 0.34514 0.34514 0.0 * CROSSFLOW JUNCTION BETWEEN LOWER INLET ADDULUS 1 AND 2 2720000 LINCR-FL SNULJUN 202000000 242000000 7.27937-2 98.0000 18.0000 00003 2720101 2720201 0.29508 0.29508 0.0 * CRUSSFLOW JUNCTION RETWEEN DOWNCOMERS 162 8 # JUNCTION BETWEEN DOWNCOMER 1.1 AND 2.1 -6 2730000 CROSFLW1 SNGLJUN 2730101 204000000 284000000 9.73328-2 98.0000 18.0000 2730201 Ő. 8.5077-2 8.5077-2 0.0 -5 * JUNCTION BETWEEN DOWNCOMER 1.2 AND 2.2 24 2750000 CROSFLW2 SNGL JUN 206000000 206000000 9.73328-2 98.0000 2750101 18.0000 00003 2750201 0 7.3113-2 7.3113-2 0.0 * JUNCTION BETWEEN DOWNCOMER 1.3 AND 2.3 100 2770000 CROSFLW3 SHGLJUN 2770101 208000000 288000000 9.73328-2 98.0000 18.0000 00003 2770201 0 5.5365-2 5.5365-2 0.0 * JUNCTION BETWEEN DOWNCOMER 1.4 AND 2.4 6 2790000 CROSFLW4 SNGLJUN 2790101 210000000 290000000 9.73328-2 98.0000 18.0000 00003 2790201 0 -0.16678 -0.16678 0.0 . INLET ANNULUS TOP VOLUME 2 2800000 INANTOP2 ANNULUS 2800001 1 2800101 0.0 2800301 0.33 1 2800401 0.0428 1 2600501 0.0 1 2800601 90.0 1 2800701 0.33 1 2800801 3.81=6 0.178 2801001 00 2801201 003 14.°55E6 556.26 0.0 0.0 0.0 1 ***** 2810000 J280-282 SNGL JUN 2810101 280000000 282000000 0.0 2810201 0 0.15614 0.15614 0.0 0.0 0.15614 0.0 **整整部整合物型进行力型的变形力量的变化力量的变体的分型的分量的变体的变化的分化的分子分子的分子分子分子的分子的分子的分子的分子的分子的分子的** * INLET A MULUS BUTTOM VOLUME 2

A-15

* DUW ICOMER 2.3 2880000 DWNCR2.3 ANNULUS 2880001 1 28801^1 0.071 1 2880301 0.958 1 2880401 0.0 1 2880501 0.0 1 2880601 -90.0 1 2880701 -0.958 1 2880801 3.81+6 0.102 1 00 2861001 2881201 003 14.97786 556.23 0.0 0.0 0.0 . JUNCTION BETWEEEN DOWNCOMER 2.3 AN 1 2.4 2690000 J2.3-2.4 SNGLJUM 2890101 288010000 29000000 0.0 0.0 0.0 00000 2890201 0 0.88045 0.82045 0.0 P DOWNCOMER 2.4 2900000 DANCR2.5 ANNULUS 2900001 1 2900101 0.071 1 2900301 0.958 1 2900401 0.0 1 2900501 0.0 1 2700601 -90.0 1 2900701 -0.958 1 2900801 3.81-5 0.102 1 2901001 00 2901201 003 14.98466 556.22 0.0 0.0 0.0 ****** . BP' KEN LOOP * REACTOR VESSEL MOZZLE - BROKEN LOOP HUT LEG 3000000 RVN-BL4L BRANCH 2 3000001 4.0-5 0.0 000 14.0-3000101 0.0634 0.0 0.0 0.0 0.0 3000102 00 000 3000200 1.276866 2.461166 3.8315-7 3001101 250010000 30000000 0.0634 1.10264 0.66160 00000 3002101 300010000 305000000 0.0 0.10050 0.10050 00000 3001201 -6.4728-7 4.2262-2 0.0 3002201 1.6459-10 3.5352-7 0.0 * HOT LEG PIPE TO REFLOND ASSIST BYPASS TEE 3050000 HLP-RAST BRANCH 3050001 1 0 3050101 0. . 34 0.698 0.0 0.0 0.0 0.0 3050102 400-5 00 3050200 14.95026 265.45 003 3051101 305010000 310000000 0.0 0.10050 0.10050 00000 3051201 2.1220-10 2.1220-10 0.0 * BROKEN LOOP OT LEG CONTRACTION -1.0 3100000 BLH-CNTR BPANCH 3100001 2 0

Jacoba Do Dug 14.75266 264.95 Jacoba Do Dug 14.7526 26.95 STEAM GENERATOR AND FUNE SIMULATOR STEAM GENERATOR AND FUNE SIMULATOR JISOLOG SGEPUN JISOLOG SGEPUN JISOLOG SGEPUN JISOLOG SGEPUN JISOLOG SISOLO ZINCE JISOLOG SISOLOG ZINCE JISOLOG ZINCE	3100101 3100102	0.0	1.424	0.0668	0.0	0.0	0.0	
STEAM GENERATIR AND PUPP SIMULATIR ************************************	3101101 3102101 3101201 3102201	380010000 310010000 -5.566-11 8.4236-10	14.95566 310000000 315000000 -6.503-11 8.7407-10	0.0328 0.0 0.0 0.0 0.0	1.24700 0.39605	0.45760 0.75363	00000	
Bisecce SG-P-UMP PIPE 3150000 SG-PUMP PIPE 3150001 0.0 S 3150001 0.0 S 3150021 0.00 S 3150022 3.260-2 S 3150203 1.0056-1 S 3150204 3.260-2 S 3150205 3.2057 S 3150206 1.00570 S 3150301 0.93100 S 3150303 0.48950 S 3150304 2.05100 S 3150305 1.47300 S 3150401 7.788-3 S 3150402 1.725-1 S 1150405 4.050-2 S 3150404 1.725-1 S 1150405 4.050-2 S 3150406 1.725-1 S 3150705 1.315070 S 3150704 0.4570 S 3150705 1.315071 S 31	# STEAH G	ENERATOR	AND PUMP 3	SIMULATOR	*********	\$3\$99999999999	00000000000	989
S150000 SG=204P FIPE S150101 0.0 6 S150201 8.365-3 1 S150202 3.260-2 2 S150203 1.056-1 3 S150205 8.365-3 7 S150205 8.365-3 7 S150205 2.05100 2 S150301 0.93100 1 S150305 2.05100 5 S150306 1.03200 7 S150306 1.03200 7 S150306 1.03200 7 S150401 7.788-3 1 S150401 7.788-3 1 S150401 7.788-3 1 S150401 7.788-3 1 S150401 7.788-3 1 S150402 8.980-2 4 S150402 8.980-2 4 S150403 8.980-2 4 S150404 1.725-1 2 S150405 8.980-2 4 S150405 8.980-2 4 S150405 8.980-2 4 S150405 8.980-2 4 S150405 8.980-2 4 S150405 8.980-2 6 S150406 4.560-2 7 S150406 4.560-2 7 S150406 4.560-2 7 S150406 4.560-2 7 S150406 -0.6570 3 S150702 2.0510 1 S150703 -2.0510 2 S150704 -0.4570 4 S150705 -2.0510 2 S150704 -0.4570 4 S150705 -2.0510 2 S150704 -0.4570 4 S150705 -2.0510 2 S150704 -0.4570 4 S150705 0.500.0 0.5000 7 S150705 0.5000 0.0500 7 S150705 0.5000 0.0500 7 S150705 0.5000 0.0500 7 S150705 0.5000 0.0500 7 S150705 0.000 0 7 S150705 0.000 0 7 S150705 0.000 0 7 S150705 0.000 0 0.00 0 0 S151204 003 14.93266 560.98 0.0 0.0 0.0 0.0 2 S151204 003 14.93266 550.98 0.0 0.0 0.0 0.0 3 S151204 003 14.93266 550.98 0.0 0.0 0.0 0.0 5 S151204 003 14.93266 550.98 0	*********	*****			********	*******	*********	0.2.11
9150101 0.0 8 9150201 0.105-1 3 9150203 1.055-1 3 9150205 8.365-3 7 9150205 8.365-3 7 9150205 8.365-3 7 9150205 8.365-3 7 9150303 0.48950 4 9150303 0.48950 4 9150305 1.47350 6 9150305 1.47350 6 9150402 1.725-1 2 9150403 8.980-2 7 9150402 1.725-1 5 9150403 8.980-2 7 9150403 1.980-2 8 9150403 90.0 7 9150403 90.0 7 9150403 90.0 7 9150403 1.2010 8 9150403 1.2010 8 91504047 1.4950-2 8 9150405 1.2140 8 9150707	3150000	SG=PUMP		PIPE				
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$\begin{array}{cccccccccccccccccccccccccccccccccccc$	3150705	1.2140	8					
3150902 16.8777 16.8777 2 3150903 0.50000 0.50000 3 3150904 16.8777 16.8777 4 3150905 0.23025 0.23025 5 3150906 2.53400 2.53400 6 3151001 00 8 3151201 003 14.948E6 564.86 0.0 0.0 0.0 1 3151202 003 14.928E6 560.98 0.0 0.0 0.0 2 3151203 003 14.928E6 560.98 0.0 0.0 0.0 3 3151204 003 14.929E6 559.98 0.0 0.0 0.0 4 3151205 003 14.929E6 558.96 0.0 0.0 0.0 6 3151205 003 14.938E6 558.98 0.0 0.0 0.0 6 3151207 003 14.957E6 556.98 0.0 0.0 0.0 7 3151207 003 14.957E6 556.98 0.0 0.0 0.0 7	3150901	4.0=3	0.0	8				
3150903 0.50000 3 3150904 16.8777 16.8777 3150905 0.23025 5 3150906 2.53400 2.53400 3150907 5.06900 7 3151001 00 8 3151201 003 14.948E6 564.86 0.0 0.0 0.0 1 3151202 003 14.928E6 560.98 0.0 0.0 0.0 2 3151203 003 14.928E6 560.98 0.0 0.0 0.0 2 3151203 003 14.928E6 560.98 0.0 0.0 0.0 2 3151204 003 14.928E6 558.98 0.0 0.0 0.0 4 3151205 003 14.927E6 559.98 0.0 0.0 0.0 5 3151205 003 14.938E6 558.98 0.0 0.0 0.0 6 3151206 003 14.957E6 556.98 0.0 0.0 0.0 7 3151207 003 14.957E6 55	3150902	16.8777	16.8777	2				
3150905 0.23025 0.23025 5 3150906 2.53400 2.53400 6 3150907 5.06900 5.06900 7 3151001 00 8	3150903	0.50000	0.50000	3				
3150906 2.53400 2.53400 6 3150907 5.06900 5.06900 7 3151001 00 8 3151201 003 14.94866 564.86 0.0 0.0 1 3151202 003 14.94866 560.98 0.0 0.0 0.0 2 3151203 003 14.92966 560.98 0.0 0.0 0.0 2 3151204 003 14.92966 559.98 0.0 0.0 0.0 4 3151205 003 14.93866 558.98 0.0 0.0 0.0 4 3151205 003 14.93866 558.98 0.0 0.0 0.0 5 3151205 003 14.93866 556.98 0.0 0.0 0.0 6 3151206 003 14.95766 556.98 0.0 0.0 0.0 6 3151207 003 14.95766 556.98 0.0 0.0 0.0 7 3151203 003 14.95766 556.98 0.0 0.0	3150905	0.23025	0.23025	4				
3150907 5.06900 5.06900 7 3151001 00 8 3151201 003 14.948E6 564.86 0.0 0.0 0.0 1 3151202 003 14.928E6 560.98 0.0 0.0 0.0 2 3151203 003 14.929E6 560.98 0.0 0.0 0.0 2 3151204 003 14.929E6 559.98 0.0 0.0 0.0 4 3151205 003 14.928E6 558.98 0.0 0.0 0.0 5 3151205 003 14.928E6 556.98 0.0 0.0 0.0 6 3151206 003 14.950E6 556.98 0.0 0.0 0.0 6 3151207 003 14.957E6 556.98 0.0 0.0 0.0 7 3151207 003 14.957E6 556.98 0.0 0.0 7 3151203 003 14.955E6 556.98 0.0 0.0 0.0 7	3150906	2.53400	2.53400	6				
3151101 00000 7 3151201 003 14.948E6 564.86 0.0 0.0 0.0 1 3151202 003 14.948E6 560.98 0.0 0.0 0.0 2 3151203 003 14.928E6 560.98 0.0 0.0 0.0 2 3151203 003 14.928E6 560.98 0.0 0.0 0.0 3 3151204 003 14.929E6 559.98 0.0 0.0 0.0 4 3151205 003 14.938E6 558.98 0.0 0.0 0.0 5 3151205 003 14.938E6 556.98 0.0 0.0 0.0 6 3151206 003 14.950E6 556.98 0.0 0.0 0.0 6 3151207 003 14.957E6 556.98 0.0 0.0 0.0 7 3151203 003 14.957E6 556.98 0.0 0.0 0.0 7 3151203 003 14.955E6 556.98 0.0 0.0 <td< td=""><td>3151001</td><td>5.06900</td><td>5.06900</td><td>7</td><td></td><td></td><td></td><td></td></td<>	3151001	5.06900	5.06900	7				
3151201 003 14.948E6 564.86 0.0 0.0 0.0 1 3151202 003 14.928E6 560.98 0.0 0.0 0.0 2 3151203 003 14.928E6 560.98 0.0 0.0 0.0 2 3151204 003 14.929E6 559.98 0.0 0.0 0.0 4 3151205 003 14.928E6 558.98 0.0 0.0 0.0 5 3151206 003 14.928E6 558.98 0.0 0.0 0.0 6 3151207 003 14.956E6 556.98 0.0 0.0 0.0 6 3151207 003 14.957E6 556.98 0.0 0.0 0.0 7 3151207 003 14.957E6 556.98 0.0 0.0 0.0 7 3151208 003 14.955E6 556.98 0.0 0.0 0.0 7	3151101	00000	7					
3151202 003 14.95866 560.98 0.0 0.0 2 3151203 003 14.92966 560.98 0.0 0.0 0.0 3 3151204 003 14.92966 559.98 0.0 0.0 0.0 4 3151205 003 14.92966 558.98 0.0 0.0 0.0 4 3151205 003 14.93866 558.98 0.0 0.0 0.0 5 3151206 003 14.95066 556.98 0.0 0.0 0.0 6 3151207 003 14.95766 556.98 0.0 0.0 0.0 7 3151207 003 14.95766 556.98 0.0 0.0 0.0 7 3151207 003 14.95566 556.98 0.0 0.0 0.0 7	3151201	003	14.94886	564.86	0.0	0.0	0.0	1
3151204 003 14.92766 559.98 0.0 0.0 4 3151205 003 14.93866 558.98 0.0 0.0 0.0 5 3151205 003 14.93866 558.98 0.0 0.0 0.0 5 3151206 003 14.95026 556.98 0.0 0.0 0.0 6 3151207 003 14.95726 556.98 0.0 0.0 0.0 7 3151207 003 14.95726 556.98 0.0 0.0 0.0 7 3151203 003 14.95526 556.98 0.0 0.0 0.0 7	3151202	003	14.908E6	560,98	0.0	0.0	0.0	2 4
3151205 003 14.938E6 558.98 0.0 0.0 0.0 5 3151206 003 14.950E6 556.98 0.0 0.0 0.0 6 3151207 003 14.957E6 556.98 0.0 0.0 0.0 7 3151207 003 14.957E6 556.98 0.0 0.0 0.0 7 3151203 003 14.955E6 556.98 0.0 0.0 0.0 7	3151204	003	14.92926	559.98	0.0	0.0	0.0	t,
3151207 003 14.95726 556.98 0.0 0.0 0.0 6 3151207 003 14.95726 556.98 0.0 0.0 0.0 7 3151203 003 14.95526 556.98 0.0 0.0 0.0 7	3151205	003	14.938E6	558.98	0.0	0.0	0.0	5
3151208 003 14.95566 556.98 0.0 0.0 0.0 8	3151207	003	14.95756	556.98	0.0	0.0	0.0	7
	3151208	003	14.95586	556.98	0.0	0,0	0.0	8

3151301	8.3150-10 :	1.0084-9	0.0	01		
3151302	1.5261-10	3.3970-10	0.0	02		
3151303	3.7289-11	3.7270-11	0.0	03		
3151304	8.9420=11	-9.763-11	2.0	04		
3151305	1.1080-10	-1-211-10	0.0	05		
3151300	0 + 1000-11	· 2972-11	0.0	07		
943455555555 9434701	5 * 0 7 3 7 - 4 1	ななななななななななな	0 6 8 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	*********		
HUT LEG	BREAK PLA	ЧE				
*********	******			*******	**********	00000000000000000000000000000000000000
3300000	HLBRKPL		VALVE			
3300101	315010000	000000000	8,3650-3	0.95883	1.0+6	00100
3300102	1.00	1.00				
3300201	0	.00000000	.00000000	0.0		
3300300	TRPYLY					
RRYSSURRYS DOMODOT	STAN STREETS		*********			
8 REACTOR	VESSEL 10	ZZLE - ERD	KEN LOCH C	OLD LEG		
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3350000	RVN-BLPL		BRA' CH			
3350001	2	0				
3350101	0.0634	0.	0.0	0.0	G.O	0.0
3350102	4.0-5	0.0	00			
3350200	003	14.90060	224,31	0 00400	1 43040	00000
2221101	2821-10000	360000000	0.0024	0.10050	0.10050	00000
3351201	-1 732-10	-1.483-10	0.0	0.10000	0100000	
3352201	-1.528-10	-1.528-10	0.0			
*****		******	计算法的 化合金合金		*****	*****
#COLD LEG	PIPE TO	REFLOOD AS	SIST BYPAS	SS TEE		
***	*****	*****	***	******	0 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	****
3400000	CLP-RABT	1.000	BRANCH			
3400001	1	0 400	0.0	0.0	0.0	0.0
3400101	0.0634	0.070	0.0	0.0	U.	V.*.
3400200	003	14.956F6	554.09			
3401101	340010000	345000000	0.0	0.10050	0.10050	00000
3401201	-1.338-10	-1.338-10	0.0			
*******	*******	**********	6666666666	the second second second second second second		
* BROKEN				\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	***	******
*****	LOOP COLD	LEG CONTRA	CTION -1.	8888888888 0		*****
	LOOP COLD	LEG CONTRA	CTION -1.1	84499444944 0 84499499999	5 * * * * * * * * * * * * * * * * * * *	00000000000000000000000000000000000000
3450000	LOOP COLD	LEG CONTRA	ACTION -1.1 NOTES	86898888888 0 8669886888	89999999999999999999999999999999999999	85000000000000000000000000000000000000
3450000 3450001 3450101	LOOP COLD BLC-CNTR 2 0-0634	LEG CONTRA	BRAUCH	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0.0	0.0
3450000 3450001 3450101 3450102	LOOP COLD 8888888888888888 BLC=CNTR 2 0.0634 4.0=5	LEG CONTRA	BRANCH	0 • 0 • 0 • 0 • 0 • 0	0.0	0.0
3450000 3450001 3450101 3450102 3450200	LDOP COLD BLC=CNTR 2 0.0634 4.0=5 003	LEG CONTRA 0.700 0.700 14.95626	0.0 053.99	0 • 0 • 0 • 0 • 0 • 0 • 0	0.0	00
3450000 3450001 3450101 3450102 3450200 3451101	LDDP CDLD BLC-CNTR 2 0.0634 4.0-5 003 345000000	LEG CONTRA 0.700 0.700 14.956E6 370000000	0.0 553.99 0.0388	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0.0 1.24700	0.0000
3450000 3450001 3450101 3450102 3450200 3451101 3452101	LDDP CDLD BLC-CNTR 2 0.0634 4.0-5 003 345000000 345010000	LEG CONTRA 0.700 0.700 14.956E6 370000000 35000000	CTION -1. BRAUCH 0.0 553.99 0.0388 0.0634	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0.0 1.24700 19.3560	0.0000
3450000 3450001 3450101 3450102 3450200 3451101 3452101 3451201	LDOP COLD BLC-CNTR 2 0.0634 4.0-5 003 345000000 345010000 -1.719-10	LEG CONTRA 0.700 0.0 14.956E6 370000000 35000000 -1.501-10	CTION -1. BRAUCH 0.0 00 553.99 0.0388 0.0634 0.0	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0.0 1.24700 19.3560	0.00 0.0 0.000 0.0000 0.0000
3450000 3450001 3450101 3450102 3450200 3451101 3452101 3451201 3452201	LDOP COLD BLC-CNTR 2 0.0634 4.0-5 003 345000000 345010000 -1.719-10 -9.748-12	LEG CONTRA 0.700 0.700 14.956E6 370000000 350000000 -1.501-10 -1.115-11	0.0 00 553.99 0.0388 0.0634 0.0 0.0	0 0 0 0 0 0 0 0 0 0 0 0 0 0	0.0 1.24700 19.3560	0.0 0.0 0.0 0.000 0.000 0.0000
3450000 3450001 3450101 3450102 3450200 3451101 3452101 3452201 3452201	LDOP COLD BLC-CNTR 2 0.0634 4.0-5 003 345000000 345010000 -1.719-10 -9.748-12	LEG CONTRA 0.700 0.700 14.95626 370000000 350000000 -1.501-10 -1.115-11	CTION =1. BRAUCH 0.0 053.99 0.0388 0.0634 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	0 0 0 0 0 0 0 0 0 0 0 0 0 0	0.0 1.24700 19.3560	44496466466666 0.0 0.0 0.0 0.00
3450000 3450001 3450101 3450102 3450200 3451101 3452201 3452201 3452201 84548484888 8 BREAK Si	LDOP COLD BLC-CNTR 2 0.0634 4.0-5 003 345000000 345010000 -1.719-10 -9.748-12 000L PIECE	LEG CONTRA 0.700 0.700 14.956E6 370000000 350000000 -1.501-10 -1.115-11	CTION =1. BRAUCH 0.0 053.99 0.0388 0.0634 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	0 + + + + + + + + + + + + + + + + + + +		**************************************
3450000 3450001 3450101 3450102 3450200 3451101 3452201 3452201 ********* * BREAK Si *********	LDOP COLD BLC-CNTR 2 0.0634 4.0-5 003 345000000 -1.719-10 -9.748-12 0.748-12 0.748-12 0.748-12 0.748-12 0.748-12 0.748-12 0.748-12 0.888000000000000000000000000000000000	LEG CONTRA 0.700 0.700 14.956E6 370000000 -1.501-10 -1.115-11	ACTION =1. BRALCA 0.0 00 553.99 0.0388 0.0634 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	0 0 0 0 0 0 0 0 0 0 0 0 0 0	0.0 1.24700 19.3560	 44444444444 644444444 644444444 644444444 644444444
3450000 3450001 3450102 3450200 3451101 3452201 3452201 3452201 3452201 845484888 8 BREAK S 848488888 8 BREAK S 848488888 8 BREAK S	LDOP COLD BLC-CNTR 2 0.0634 4.0-5 003 345000000 -1.719-10 -9.748-12 ********* PODL PIECE ********* BRK-SP 0.0	LEG CONTRA 0.700 0.700 14.95656 370000000 -1.501-10 -1.115-11 ********* SNGLVOL 0.762	CTION -1. BRAUCH 0.0 0553.99 0.0388 0.0634 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	0 0 0 0 0 0 0 0 0 0 0 0 0 0	0.0 1.24700 19.3560 200000000000000000000000000000000000	0.0 0.0 0.0 0.0 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.0000 0.00
3450000 3450001 3450101 3450102 3450200 3451201 3452201 ********* * BREAK Si ********* 3500000 3500102	LDOP COLD 84888888888 BLC=CNTR 2 0.0634 4.0=5 003 345000000 -1.719=10 -9.748=12 8488888888 PONL PIECE 8488888888 BRK=SP 0.0 4.0=5	LEG CONTRA 0.700 0.700 14.956E6 370000000 =1.501=10 =1.115=11 ********* SNGLVOL 0.762 0.0	CTION -1. SERALCH 0.0 00 553.99 0.0388 0.0634 0.0 0.0 SERESEE SERESEE SERESEE 0.023360 00	0.0 0.45760 9.01672 0.0 0.0 0.0 0.0	0.0 1.24700 19.3560 200000000000000000000000000000000000	0.0 0.0 0.0 0.0 0.000 0.000 0.000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.00000 0.000000
3450000 3450001 3450102 3450200 345101 3452101 3452201 855200 8552000	LDOP COLD 84888884888 BLC=CNTR 2 0.0634 4.0=5 003 345010000 -1.719=10 -9.748=12 8488888888 PONL PIECE 8888888888 BRK=SP 0.0 4.0=5 003	LEG CONTRA 0.700 0.700 14.956E6 370000000 =1.501=10 =1.115=11 ********* SNGLV0L 0.762 0.0 14.956E6	CTION =1. SPRALC D.0 00 553.99 0.0388 0.0634 0.0 0.0 SSR SPRESS 0.023360 00 552.47	0.0 0.45760 9.01672 0.0 0.0 0.0 0.0	раненалана 0.0 1.24700 19.3560 лерарорана самерарорана 0.0	0.0 0.0 0.0 0.000 0.000 0.000 0.000 0.000 0.000 0.00 0.00 0.00
3450000 3450001 3450101 3450102 3450200 3451101 3452201 3452201 3452201 3452201 ********* * BREAK Si ********* 3500000 3500102 3500200 ********	LDOP COLD 84844448 BLC-CNTR 2 0.0634 4.0-5 003 345010000 -1.719-10 -9.748-12 84504000 -1.719-10 -9.748-12 84504000 BRK-SP 0.0 4.0-5 003 885666888 0.0 4.0-5 0.0 0.0 4.0-5 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	LEG CONTRA 0.700 0.700 14.956E6 370000000 350000000 -1.501-10 -1.115-11 0.762 0.0 14.956E6 0.762 0.0 14.956E6	CTION =1. SPRALC D.0 00 553.99 0.0388 0.0634 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	0 0 0 0 0 0 0 0 0 0 0 0 0 0	ранечалана аккачалана 0.0 1.24700 19.3560 кекералена салеранена 0.0 аванерана	 6444444444444444 644444444 644444444 6444444444 6444444444 6444444444 6444444444 6444444444 6444444444 6444444444 64444444444 64444444444 6444444444444 644444444444 6444444444444444444444444444444444444
3450000 3450001 3450101 3450102 3450200 3451101 3452201 3452201 3452201 8468888888 8 BREAK Si 8684888888 8 BREAK Si 8684888888 3500000 3500102 3500200 8488888888 8 COLD LEC	LDOP COLD BLC-CNTR 2 0.0634 4.0-5 003 345010000 -1.719-10 -9.748-12 0.0 4.0-5 0.0 4.0-5 0.0 4.0-5 0.0 4.0-5 0.0 BREAK PL	LEG CONTRA 0.700 0.700 14.956E6 370000000 -1.501-10 -1.115-11 ********* SNGLVOL 0.762 0.0 14.956E6 ********	CTION =1. SPRALC D.0 00 553.99 0.0388 0.0634 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	0 0 0 0 0 0 0 0 0 0 0 0 0 0		
3450000 3450001 3450101 3450102 3450200 3451101 3452201 3452201 3452201 3452201 3452201 3452201 3452201 3500102 3500102 3500200 3500102 3500200 3500200 3500200	LDOP COLD BLC-CNTR 2 0.0634 4.0-5 003 345010000 -1.719-10 -9.748-12 ********* BRK-SP 0.0 4.0-5 003 *********************************	LEG CONTRA 0.700 0.700 14.956E6 370000000 350000000 -1.501-10 -1.115-11 ********* SNGLVOL 0.762 0.0 14.956E6 ********	CTION =1. SERALCH D.0 00 553.99 0.0388 0.0634 0.0 0.0 SSEE 0.023360 00 552.47 SEE SEE SEE SEE SEE SEE SEE SE	0 0 0 0 0 0 0 0 0 0 0 0 0 0		 644444444444 644444444 644444444 644444444 6444444444 6444444444 6444444444 6444444444 64444444444 64444444444 64444444444 6444444444444444444444444444444444444

3650102	0.84	0.84					
3650201	0	.00000000	.00000000	0.0			
3650300	TPPVLV						
3650301	510						
教授保持委任务条件	****	经资料资料资料资格	******	******		40000000000000	6
* REFLOOD	ASSIST B	YPASS PIPI	NGCOLD	LEG SIDE			
***	*****	*****		*****	********		25
3700000	RABS-C-L		PIPE				
3700001	3						
3700101	0.0388	2					
3700102	0.0776	3					
3700201	0.0388	2					
3700301	0.0	3					
3700401	0.0279	1					
3700402	0.070	2					
3700403	0.1165	3					
37, 1601	90.	1					
3700602	0.0	3					
3700701	0.64	ĩ					
3700702	0.0	2					
3700801	4-0-5	0.0					
3700901	0.25	0.28	i.				
3700902	0.84	0.84	-				
3701001	00	3	6				
3701101	000000	-					
3701201	00000	14.05452	618 04				
3701202	000	10 05000	202,90	0.0	0.0	0.0 1	
3701203	003	10 05000	202.90	0.0	0.0	0.0 2	
3701300	003	T## 45550	265.41	0.0	0.0	0.0 3	
3701301	-1 401-10	-1 202 10					
3701302	-1:471-10	-0 301-11	0.0	C1			
0000000 000000000000000000000000000000	-7.0-2-11 		U.U.	92			
* REELODD	ACCICT ON	VDACC VALUE	- - -	**********	**********	상 등 왕 한 철 중 철 중 철 중 철 중 철 중 철 중 철 중 철 중 철 중 철	p.
SSSSSSSSS	0 101060 	REPERT					
3750000	DAD-VI V	**********	14444444444444444444444444444444444444	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0 P # P & D & D & D & D & D & D & D & D & D &	***	R
3750101	AZOOLODOO	300000000	VALVE				
8750201	310010000	200000000	00000000	0.0	0.0	00000	
3750300	TREVIN		.00000000	0.0			
3750301	505						
60405602a	JUL						
& REELDON	ACCICT ON	DASS DIDIA	- UUT -		299999999999999999	00000000000000000000000000000000000000	P
BBBBBBBBBBBB	1010101 1010101	CASSEREELE	VJ - MUL L	EO SIDE			
3800000	DADC-U-I		010- 010-	**********	20000000000	*****	k., .
3800001	1 1000-11 L		ring				
3600101	0 0776						
3800102	0.0388	3					
3800201	0.0388	5					
3800301	0.0	4					
3800401	0.1165	1					
3800402	0.023	5					
3800403	0.0489	9					
3800601	0.0	1					
3800602	0.0	5					
3800603	-90-	3					
3800701	0.0	1					
3800702	0.0	2					
3800703	-0-60	3					
3800801	4-0-5	0.0	1				
3800901	0.84	0.84	Ť				
3800902	0.28	0.28	5				
3801001	00	3					
3801101	00000	2					

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 3801201
 003
 14.945E6
 565.97
 0.0
 0.0

 3801202
 003
 14.946E6
 565.97
 0.0
 0.0

 3801203
 003
 14.948E6
 565.96
 0.0
 0.0
 0.0 2 0.0 0.0 3 3801300 0 3601301 -3.448-11 -3.448-11 0.0 01 3801302 -4.128-11 -5.256-11 0.0 02 · PRESSURIZER ▹ SURGE LINE PCS SIDE BRANCH 4000000 SRGLPCS 4000001 2
 4000001
 2
 0

 4000101
 0.00145
 2.300
 0.0

 4000102
 4.0-5
 0.0
 00

 4000200
 003
 14.93826
 614.60

 4001101
 11000000
 40000000
 0.0
 Ó. 0.0 90.0 0.54 0.93000 0.93000 00100 4002101 400010000 405000000 0.0 4001201 -5.9858-3 -8.8060-3 0.0 4002201 -5.9860-3 -5.9860-3 0.0 ******* * PRESSURIZER SURGE LINE 4050000 SRG-PZR PIPE 4050001 2 4050101 0.00145 2 4050201 0.00145 1 4050301 2.30 2 4050401 0.0 2 90.0 4050601 2 2
 4050701
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 4050801
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 4051001
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 14.935E6
 63
 4050701 0.30 14.935E6 614.41 0.0 0.0 0.0 14.934E6 614.42 0.0 0.0 0.0 0.0 1 2 4051202 003 4051300 0 4051301 -5.9830-3 -5.9860-3 0.0 01 ****** * PRESSURIZER SURGE LINE VALVE *** 4100000 PZR-VLV VALVE 4100101 405010000 415000000 0.0 0.93000 0.93000 00100 -5.9861-3 -5.9861-3 0.0 4100201 0 4100300 TRPVLV 4100301 501 ****** * PRESSURIZER VESSEL PIPE 4150000 PZRVESEL 4150001 7 4150101 0.0 2 4150102 0.5653 5 0.0 7 4150103 6 4150201 0.0 4150301 0.1815 1 0.1524 2 4150302 3 4150303 0.3967 0.5289 4 4150304 14 4150305 0.3967 4150306 0.1943 6

4150307 4150401 4150402 4150403 4150404 4150405 4150501 4150601 4150801	0.1029 0.0684 0.0838 0.0 0.0732 0.0142 0.0 90.0 4.0-5	71255677770.0	7				
4151001	00	7					
4151101	00000	14 03054	614 42	0.0	0.0	0.0	
4151202	000	14.93166	1.5835E6	2.401566	1.6479-9	0.0	2
4151203	000	14.93026	1.583766	2.461526	5.5001-7	0.0	3
4151204	000	14.92786	1.5036E6	2.461686	0.22596	0.0	4
4151205	000	14.92686	1.5834E6	2.461626	1.0	6.0	5
4151206	000	14.92526	1.023416	2.451020	1.0	0.0	7
4151300	000	74.76360	1.903.00	C*4070C0	1.0		
4151301	1.0230-6	3.0885-5	0.0	01			
4151302	7.0120-7	7.0512-3	0.0	02			
4151303	6.2771-7	0.32550	0.0	03			
4151304	-0,23616	9,3043-6	0.0	04			
4151305	-1.1303-3	3 + 1249=0	0.0	05			
4491900	0.0000000000000000000000000000000000000	0.0000000000000000000000000000000000000	10000000000000000000000000000000000000	0000000000000			
* TOP VOL	UNE PRESSU	RIZER					
000000000	2 ~ 4 ~ 4 ~ 4 ~ 4 ~ 4 ~ ~ ~ ~ ~ ~ ~ ~ ~		10000000000000000000000000000000000000	0 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	000000000000000000000000000000000000000	00000000000	04444
4200000	TDPV-PZR		BRANCH				
4200001	1	0 1020	0.0142	0.0	90.0	0.1029	
4200102	4.0=5	0.0	00	4.4			
4200200	000	14.925E6	1.583486	2.4516E6	1.0		
4201101	415010000	420000000	0.0	0.0	0.0	00000	
4201201	-6.7300-4	8.6127-6	0.0				LARAD
\$ DUSV	***********	**********	* * * * * * * * * * * * * * *			*******	PARAN
888888888			********		*****	*******	
4250000	PCK-VLV		VALVE				
4250101	420010000	81000000	9.0-5	0.0	0.0	00100	
4250201	0	*00000000	.00000000	0.0			
4250300	A91						
*****	0.4						
* STEAM	GENERATOR	SECONDAR	Y SIDE		*****	*****	24244
*****	****	0.000000000000000000000000000000000000	1000 000 000 000 000 000 000 000 000 00		/ 各些各种的的的故障的	*****	1989999
9 TOP 07	DOWNCOMEN	(CUUILEI	DE FEIMARI	Y SEPRATUR	1		
5000000	SPR-OUT		SEPARATR				
5000001	3	0					
5000101	0.0	0.8288	1.0277	0.0	90.0	0.8288	
5000102	4.0-5	0.7697	00		0.05437		
5000200	5000	5.519226	1.118956	2.593026	0.0	00100	
5002101	500010000	505000000	0.0	0.0	0.0	00100	
5003101	51501000	500000000	0.196	0.0	0.0	00100	
5001201	0.88915	2.4000	0.0				
5002201	0.45877	-0.77061	0.0				
5003201	2.4507	2.9618	0.0				
& LINFR	SEDBARDARD SEDBARDARD	FCTION =1.0	ដ្ឋជាជាត្មនានាមម (*********	THE REPORT OF		

	F. 75 FL 25 AL 25 AL 26 AL 25 AL 24	and data and and and one of the					
5050000	IUDLCCOD	**********	动动物物动物 动动	····································	*****	*****	60000
5050001	Lanestri		BRANCH				
SCROID4	4	0					
5050101	0.0	0.8288	1.0085	0.0	-90.0	-0.2223	
2050102	4.0-5	0.72845	00			-0.0450	
5050200	003	5.5227E6	543.31				
5051101	505010000	507000000	0.0	0.0	0.0		
5051201	0.13345	0.13345	0.0	N V	0.0	00100	
*****			~ * ·				
5070000	I WR-SEDE		SOAL PUL				
5070001	A CONTRACTOR		ORANCH				
5070101	÷ •	0.0000					
5070100	0.0	0.8288	1.0085	0.0	-90.0	+0.8285	
2010102	4 • 0 = 5	0.72845	20				
2010200	093	5.529086	543.31				
5071101	507010000	505000000	0.0	0.0	0.0	00100	
5071201	0.44778	0.44778	0.0		~ * ·	00100	
****		*********	555955555				
* FEED IN	ET VOLUME		*		145898989999	5. 行行合约合约合合合合合	40000
*********	0040000000						
5080000	FF1K-VDI			1 教育教育会会教育会会	······································	4. 中华的学校学校学校	教教教教徒
5080001	A LINE AND		OMA CM				
Soacto:	*	0					
2000101	0.0	0.6096	0.22107	0.0	+90.0	-0.4004	
2080102	4.0-5	0.163697	00			-0.0030	
5080200	003	5.5343F6	535.37				
5081101	508010000	510000000	0.0	0.0	0.0		
5081201	0.79141	0.79141	0.0	0.4 V	0.0	00100	
********	SEBEEEBBERN.		VaU				
# STEAM OF	NERATOR I		********	*******	******	特拉斯劳劳拉特	44444
******	CARARANANA L	A A A A A A A A A A A A A A A A A A A					
5100000	COTO DUO	**********	5.公长业务资格资格资格	教堂堂祭堂堂祭堂	*****	*****	
5100000	SULKAUMA		ANNULUS				
2100001	2						
2100101	0.000						
* * * * * * *	Vacac	2					
5100201	0.0	2					
5100201 5100301	0.0	2					
5100201 5100301 5100401	0.00	2 3 3					
5100201 5100301 5100401 5100601	0.252	1 N N N N N					
5100201 5100301 5100401 5100601 5100701	0.0 0.6096 0.0 -90.0	223333					
5100201 5100301 5100401 5100601 5100701 5100801	0.0 0.6096 0.0 -90.0 -0.6096	33333					
5100201 5100301 5100401 5100601 5100701 5100801	0.0 0.6096 0.0 -90.0 -0.6096 4.0-5	2 3 3 3 0.10793	3				
5100201 5100301 5100401 5100601 5100701 5100801 5100901	0.0 0.6096 0.0 -90.0 -0.6096 4.0-5 C.0	2 3 3 3 0.10793 0.0	3				
5100201 5100301 5100401 5100601 5100701 5100801 5100901 5100901	0.000.0000.0000000000000000000000000000	2 3 3 3 0.10793 0.0 3	3				
5100201 5100301 5100401 5100601 5100701 5100801 5100901 5104001 5101101	0.0 0.6096 0.0 -90.0 -0.6096 4.0-5 0.0 00 00000	2 3 3 3 0.10793 0.0 3 2	32				
5100201 5100301 5100401 5100601 5100701 5100801 5100901 510,001 5101101 5101201	0.0 0.6096 0.0 -90.0 -0.6096 4.0-5 (.0 00 00000 003	2 3 3 0.10793 0.0 3 2.5388E6	3 2 535.41	0.0	0.0		
5100201 5100301 5100401 5100601 5100701 5100801 5100901 510,001 5101201 5101201 5101202	0.0 0.6096 0.0 -90.0 -0.6096 4.0-5 0.0 00 00000 003 003	2 3 3 3 0.10793 0.0 3 2 5.5388E6 5.5434E6	3 2 535.41 535.46	0.0	0.0	0.0	1
5100201 5100301 5100401 5100601 5100701 5100801 5100901 5101201 5101201 5101202 5101203	0.0 0.6096 0.0 -90.0 -0.6096 4.0-5 0.0 00 00000 003 003	2 3 3 3 0.10793 0.0 3 5.5388E6 5.5434E6 5.5481E6	3 2 535.41 535.46 535.50	0.00	0.0	0.0	12
5100201 5100301 5100401 5100601 5100701 5100801 5100901 5101201 5101201 5101202 5101203 5101300	0.0 0.6096 0.0 -90.0 -0.6096 4.0-5 (.0 00 00000 003 003 003	2 3 3 3 3 0.10793 0.0 3 5.5388E6 5.5434E6 5.5481E6	3 2 535.41 535.46 535.50	0.0 0.0 0.0	0.0 0.0 0.0	0.0 0.0 0.0	123
5100201 5100301 5100401 5100601 5100801 5100901 5101001 5101201 5101201 5101202 5101203 5101300 5101301	0.0 0.6096 0.0 -90.0 -0.6096 4.0-5 (.0 00 00000 003 003 003 003 003	2 3 3 3 0.10793 0.0 3 2 5.5388E6 5.5434E6 5.5481E6 5.5481E6	3 2 535.41 535.46 535.50	0.0	0.0 0.0 0.0	0.0 0.0 0.0	123
5100201 5100301 5100401 5100601 5100701 5100801 5100901 5101201 5101201 5101202 5101203 5101300 5101301 5101302	0.0 0.6096 0.0 -90.0 -0.6096 4.0-5 (.0 00 00000 003 003 003 003 0.79148 0.79148	2 3 3 3 3 0.10793 0.0 3 2 5.5388E6 5.5434E6 5.5481E6 0.79148	3 2 535.41 535.46 535.50 0.0	0.0 0.0 0.0	0.0 0.0 0.0	0.0 0.0 0.0	123
5100201 5100301 5100401 5100601 5100801 5100901 5101001 5101201 5101202 5101203 5101300 5101301 5101302	0.232 0.0 0.6096 0.0 -90.0 -0.6096 4.0-5 (.0 00 00000 003 003 003 003 003 0 0.79148 0.79155	2 3 3 3 0.10793 0.0 3 2 5.5388E6 5.5434E6 5.5481E6 0.79148 0.79155	3 2 535.41 535.46 535.50 0.0 0.0	0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0	0.0 0.0 0.0	123
5100201 5100301 5100401 5100601 5100801 5100901 5101201 5101201 5101202 5101203 5101300 5101301 5101302	0.232 0.0 0.6096 0.0 -90.0 -0.6096 4.0-5 (.0 00 00000 003 003 003 003 003 003 003	2 3 3 3 0.10793 0.0 3 2 5.5388E6 5.5434E6 5.5481E6 0.79148 0.79155	3 2 535.41 535.46 535.50 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0	0.0	123
5100201 5100301 5100401 5100601 5100701 5100901 510101 5101201 5101201 5101202 5101203 5101300 5101301 5101302	0.232 0.0 0.6096 0.0 -90.0 -0.6096 4.0-5 (.0 00 00000 003 003 003 003 003 003 003	2 3 3 3 0.10793 0.0 3 2 5.5388E6 5.5434E6 5.5481E6 0.79148 0.79155 **********	3 2 535.41 535.46 535.50 0.0 0.0 0.0 0.0 80866886880 BDILER	0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0	0.0	123
5100201 5100301 5100401 5100601 5100701 5100901 510101 5101201 5101201 5101202 5101203 5101300 5101301 5101302 ***********	0.0 0.6096 0.0 -90.0 -0.6096 4.0-5 (.0 00 00000 003 003 003 003 003	2 3 3 3 0.10793 0.0 3 2 5.5388E6 5.5434E6 5.5481E6 0.79148 0.79155 ********** SOMER TU	3 2 535.41 535.46 535.50 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0	0.0	123
5100201 5100301 5100401 5100601 5100801 5100901 5101201 5101201 5101202 5101203 5101300 5101301 5101302 *********** JUNTION **********	0.232 0.0 0.6096 0.0 -90.0 -0.6096 4.0-5 (.0 00 003 003 003 003 003 003 003 003 00	2 3 3 3 0.10793 0.0 3 2 5.5388E6 5.5434E6 5.5481E6 0.79148 0.79155 ********** SOMER TU	3 2 535.41 535.46 535.50 0.0 0.0 0.0 0.0 0.0 800000000000000	0.0 0.0 0.0 0.0 0.0 0.1 0.2 0.2 0.2 0.2 0.2 0.2 0.2 0.2 0.2 0.2	0.0	0.0	123
5100201 5100301 5100401 5100601 5100701 5100901 5101201 5101201 5101202 5101203 5101300 5101300 5101302 ********** JUNTION ********** 5130000 5130101	0.0 0.6096 0.0 -90.0 -0.6096 4.0-5 (.0 00 00 00 00 00 00 00 00 00	2 3 3 3 0.10793 0.0 3 2 5.5388E6 5.5434E6 5.5481E6 0.79148 0.79155 ********* 50MER TU **********	3 2 535.41 535.46 535.50 0.0 ********* BDILER ******** SNGLJUN 0.0	0.0 0.0 0.0 01 02	0.0 0.0 0.0 0.0	0.0	123
5100201 5100301 5100401 5100601 5100801 5100901 5101201 5101201 5101202 5101203 5101300 5101300 5101302 ********** JUNTION ********** 5130000 5130101 5130201	0.0 0.6096 0.0 -90.0 -0.6096 4.0-5 (.0 00 00000 003 003 003 003 003	2 3 3 3 0.10793 0.0 3 2 5.5388E6 5.5481E6 0.79148 0.79155 ********* SOMER TU ********** 515000000 0.79161	3 2 535.41 535.46 535.50 0.0 0.0 ********** BDILER ********* SNGLJUN 0.0 1.0727	0.0 0.0 0.0 01 02 ********************************	0.0 0.0 0.0 0.0	0.00 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00	123
5100201 5100301 5100401 5100601 5100801 5100901 5101201 5101201 5101202 5101203 5101300 5101300 5101302 *********** 5130000 5130101 5130201 ********	0.232 0.0 0.6096 0.0 -90.0 -0.6096 4.0-5 (.0 00 003 003 003 003 003 003 003 003 00	2 3 3 3 0.10793 0.0 3 2 5.5388E6 5.5481E6 0.79148 0.79155 ********* 50MER TU ********* 515000000 0.79161	3 2 535.41 535.46 535.50 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 01 02 ********************************	0.0 0.0 0.0 0.0 17.5	0.00 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	123
5100201 5100301 5100401 5100401 5100701 5100901 5101201 5101202 5101202 5101202 5101300 5101301 5101302 ********** 5130000 5130101 5130201 ***********	0.0 0.6096 0.0 -90.0 -0.6096 4.0-5 (.0 00 00 00 00 00 00 00 00 00	2 3 3 3 0.10793 0.0 3 2 5.5388E6 5.5434E6 5.5481E6 0.79148 0.79155 ********* 50MER TU ********** 515000000 0.79161 *******	3 2 535.41 535.46 535.50 0.0 0.0 ********** BDILER ********* SNGLJUN 0.0 1.0727	0.0 0.0 0.0 02 *************************	0.0 0.0 0.0 0.0 17.5	0.00 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	123
5100201 5100301 5100401 5100401 5100701 5100901 5101201 5101202 5101202 5101202 5101300 5101301 5101302 ************ 5130000 5130101 5130201 *************	0.0 0.6096 0.0 -90.0 -0.6096 4.0-5 (.0 00 00000 003 003 003 003 003	2 3 3 3 0.10793 0.0 3 2 5.5388E6 5.5434E6 5.5481E6 0.79148 0.79155 ********* 50MER TU ********** 515000000 0.79161 **********	3 2 535.41 535.46 535.50 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 02 02 02 02 02 02 02 02 02 02 02 02 02	0.0 0.0 0.0 0.0 17.5	0.00 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.	123
5100201 5100301 5100401 5100401 5100701 5100901 5101201 5101201 5101202 5101202 5101300 5101301 5101302 *********** 5130000 5130101 5130201 ************ 5150000	0.0 0.6096 0.0 -90.0 -0.6096 4.0-5 (.0 00 00000 003 003 003 003 003	2 3 3 3 0.10793 0.0 3 2 5.5388E6 5.5434E6 5.5481E6 0.79148 0.79155 ********** 50MER TU ********** 515000000 0.79161 *********	3 2 535.41 535.46 535.50 0.0 ********* BDILER ******** SNGLJUN 0.0 1.0727 ********	0.0 0.0 0.0 02 02 02 02 02 02 02 02 02 02 02 02 02	0.0 0.0 0.0 0.0 17.5 17.5	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	1 2 3 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9
5100201 5100301 5100401 5100401 5100701 5100901 5101201 5101201 5101202 5101202 5101300 5101301 5101302 *********** 5130000 5130101 5130201 ************************************	0.0 0.6096 0.0 -90.0 -90.0 -0.6096 4.0-5 C.0 00 00000 003 003 003 003 003	2 3 3 3 0.10793 0.0 3 2 5.5388E6 5.5434E6 5.5481E6 0.79148 0.79155 ********* SOMER TU ********* 515000000 0.79161 *********	3 2 535.41 535.46 535.50 0.0 ********** BOILER ********** SNGLJUN 0.0 1.0727 *********	0.0 0.0 0.0 01 02 02 00 02 00 02 00 00 00 00 00 00 00	0.0 0.0 0.0 0.0 17.5 17.5	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.000 0.0000 0.0000	12 3 .0000 .0000 .0000 .0000
5100201 5100301 5100401 5100401 5100701 5100901 5101201 5101201 5101202 5101202 5101300 5101300 5101301 5101302 *********** 5130000 5130101 5130201 ************************************	0.232 0.0 0.6096 0.0 -90.0 -0.6096 4.0-5 0.0 00000 003 003 003 003 003 003 003 0	2 3 3 3 0.10793 0.0 3 2 5.5388E6 5.5434E6 5.5481E6 0.79148 0.79155 ********** SOMER TU ********** 515000000 0.79161 *********	3 2 535.41 535.46 535.50 0.0 0.0 0.0 0.0 0.0 801LER 806084888 806LJUN 0.0 1.0727 8888888888 8000 1.0727 8888888888 8000 1.0727 8888888888 8000 1.0727	0.0 0.0 0.0 01 02 0000000000000000000000	0.0 0.0 0.0 0.0 17.5 17.5	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.000 0.000 0.000	12 3 .000 0 .000 0 .0000 0 .00000 0 .00000000
5100201 5100301 5100401 5100401 5100701 5100901 5101201 5101201 5101202 5101202 5101300 5101301 5101302 ********** 5130000 5130101 5130201 ************* 5130000 5130101 5150101 5150102	0.0 0.6096 0.0 -90.0 -90.0 -0.6096 4.0-5 0.0 00000 003 003 003 003 003 0	2 3 3 3 0.10793 0.0 3 2 5.5388E6 5.5481E6 5.5481E6 5.5481E6 0.79148 0.79155 ********** 50MER TU ********** 515000000 0.79161 *********	3 2 535.41 535.46 535.50 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 02 02 02 02 02 02 02 02 02 02 02 02 02	0.0 0.0 0.0 0.0 17.5	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	123 99999 99999 99999 99999
5100201 5100301 5100401 5100401 5100701 5100901 5101201 5101202 5101202 5101202 5101300 5101300 5101301 5101302 ********** 5130000 5130101 5130201 *********** 5150000 5150101 5150102 5150102	0.232 0.0 0.6096 0.0 -90.0 -90.0 -0.6096 4.0-5 0.0 00000 003 003 003 003 003 003 003 0	2 3 3 3 0.10793 0.0 3 2 5.5388E6 5.5481E6 5.5481E6 0.79148 0.79155 ********** 50MER TU ********** 515000000 0.79161 *********	3 2 535.41 535.46 535.50 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 02 02 02 02 02 02 02 02 02 02 02 02 02	0.0 0.0 0.0 0.0 17.5	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.000 0.000 0.000	12 3 4 8 8 8 4 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8

5150301	1.8288	4				
5150302	0.8288	6				
5150401	0.0	6				
5150601	60.0	4				
5150602	90.0	6				
5150701	0.6096	4				
\$150702	0.8288	6				
5150801	4.0-5	0.0234	4			
5150862	4-0-5	0.587423				
5150803	4.0-5	0.6096	é.			
5150901	4.05	4.05	L.			
5150902	0.0	0.0				
5151001	00	4	*			
5151101	00000	à ·				
5151501	00000	R 566356	3 173854	3 503/52	A 31179	2 A
5151000	000	2 + 2 4 4 0 5 0 5 + 5 5 5 7 - 2	1 1 7 2 9 5 5	2 + 373450 5 + 534552	O ERCOL	0.4V 1
5151303	000	2 8 2 8 7 1 5 0 8 8 5 6 7 8 7	エネエリアリロロー	2:272250	0 40000	144 C
2707600	000	2+224/10 5 800001	1+117160	2.070020	0,00070	0.0
2121204	000	2.240720	1+1/9000	2.543056	U. 14021	0.0
2101200	000	D. D. 2. 37 E. E.	1+179256	2.593010	0.70000	0+0
2101206	000	5.251450	7*7/4769	2.393020	0.11899	Q*0 6
5151300	0					
2121201	1.0245	1.3191	0.0	01		
5151302	1.4999	2.0197	0.0	02		
5151303	1.*9438	2.7519	0.0	03		
5151304	2.3241	3.2080	0.0	04		
5151305	2.4073	2,9755	0.0	05		
*****	2. 在 在 在 中 中 中 中 中 中	· · · · · · · · · · · · · · · · · · ·	2 计存载分析存在存在	***	000000000000000	2 学校会会校校会校校会会会
* TOP OF	RISER(INS)	DE SHROND,	ABOVE TUB	ES)		
*****		2 ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~	10000000000000000000000000000000000000	****	*************	5. 操作的存在存在存在存在存在
5200000	SEPAR-IN		BRANCH			
5200001	1	0				
5200101	0.27871	0.718	0.0	0.0	90.0	0.718
5200102	4.0-5	1.0827	00			
5200200	002	5.5189E6	1.0			
5201101	520010000	525000000	0.0	0.0	0.0	00100
5201201	2.2848	2.4001	0.0			
***	****	· ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~	*****	*******	********	44844444444444444
* BELOW MI	ST EXTRACT	OR ABOVE	TOP OF S	HROND IN S'	FEAM DOME	
***	·***	· * * * * * * * * * * * * * * * * * * *	*****	***	****	2.你你你你你你你你你你你你
5250000	BUTSTMOM		BRANCH			
5250001	1	0				
5250101	1.5886	0.762	0.0	0.0	90.0	0.762
5250102	4.0-5	0.64417	00			
5250200	002	5.518766	1.0			
5251101	525010000	530	0.0	0.8	0.8	00000
5251201	7.8662	14.433	0.0			
*********				******		
* MIST EXT	RACTOR AN	ID STEAM C	EN OUTLET	PIPE TO SO	1V	
******	*******		********	***		*********
5300000	STOM/PIP		SNGLVOL			
5300101	0.04635	25.07.	0.0	0.0	0.0	0.0
5300102	4.0=5	0.0	00			
5300200	000	5.511166	1,1785EA	2-5936E6	0.99999	
*****		****				
AND STEAL	CONTROL V	ALVE 000				
********	000000000000000000000000000000000000000	******				
5500000	STONYA	SNGL HIN				
5500101	530010000	555000000	0-003667	0.0	0.0	01000
5500201	0	69.717	182.67	0.0		44444
*******		000000000000	0.0			
aba DIDE	DOWNSTREAL	OF SCU	8.8			
SPARSAASAA	SSSSSSSSSSSS	000000000000	13-6			

5550000	CHD-INLT	SNGLVOL				
5550101	0.06557	54.44	0.0	0.0	0.0	0.6
5550200	4.6-2	0.0	00			
******	0000	2:2U02E6	1.178326	2.593766	0.99960	
APA FLO	W PATH TO	THE ALE CO	DECERTERRY	200 C C C C C C C C C C C C C C C C C C		
*******	********	******	88088888888			
5600000	CDACCO	SHELJUN				
5600101	55501000	0 56500000	0 0.0	0.0	0.0	
2600201	0	0.87374	10.225	0.0	~.~	01100
899999999 804 110	·····································	****	8 \$			
ARRAGAR	CHULED CH	NDENSER #	4 4 4			
5650000	CUNPUED	59999999999999999999999999999999999999	0 D			
5650101	0.21477	17 67				
5650102	4.5-5	11.00	0.0	0.0	0.0	0.0
5650200	002	510	00			
5650201	-0.0	5.507254	1.0			
5650202	0.0	5.507256	1.0			
5650203	0.51724	5.510456	1.0			
5650204	0.68966	5.523456	1.0			
5650205	1.03448	5.5364E6	1.0			
5650206	1.55172	5.5559E6	1.0			
5650207	1.89655	5.5657E6	1.0			
5450205	2.41379	5.5754E6	1.0			
5650209	2 . 75362	5.5754E6	1.0			
5650211	2.93103	5.0722E6	1.0			
5650212	3.10345	2.2657E6	1.0			
5650213	4.13703	D=0027E6	1.0			
5650214	4-82759	5 510420	1.0			
5650215	5.17241	5.490054	1.0			
5650216	5.68966	5.477956	1.0			
5650217	6.37931	5.442156	1.0			
5650218	6.89655	5.422656	1.0			
5650219	7.58621	5.4096E6	1.0			
5650220	8.44828	5.3966E6	1.0			
2650221	9.31034	5.3933E6	1.0			
2650222	10.6897	5.4031E6	1.0			
2020223	11.2069	5.3998E6	1.0			
5650226	12.5862	5.3901E6	1.0			
5650226	19:0207	5.3803E6	1.0			
5650227	17.5862	5 367354	1.0			
5650228	20.0000	5 360004	1.0			
5650229	22.5862	5.357666	1.0			
5650230	25.0000	5.351166	1.0			
5650231	27.4138	5.3478E6	1.0			
5650232	30.0000	5.3446E6	1.0			
5650233	120.000	5.2196E6	1.0			
****	****	****	₩ 0+			
WRA MAIN	FEED WATE	R VALVE #	00			
5700000	**************************************	·····································	6 P			
5700101	57500000	(MDPJUN				
5700200	1	510	0.05			
5700201	-0.0	18 834	0.0			
5700202	0.0	18,824	0.0	0.0		
5700203	0.17341	18.824	0.0	0.0		
5700204	0.34682	14,743	0.0	0.0		
5700205	0.52023	9.6836	0.0	0.0		
5700206	0.69364	7.2827	0.0	0.0		

5700207	0.86705	3.7906	0.0	0.0		
5700208	1.04046	3.1557	0.0	0.0		
5700209	1.21387	2.2033	0.0	ñ. ñ		
5700210	1. 30758	1 5684	0.0	× • •		
5700511	1 . 20120	742004	0.0	0.0		
ETRADIA	1.13410	0.70049	0.0	0.0		
5700212	2.08092	0.11416	0.0	0.0		
5700213	2.60116	0.61603	0.0	0.0		
5700214	5.02890	0.45730	0.0	C.0		
5700215	7.63006	0.45730	0.0	0.0		
5700216	120.000	0.45730	0.0	0.0		
****	*****	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	000000			
ANA MAKE	UP FEED ST	CORAGE TANK	600			
	000000000000		000000			
5750000	FFD-TANK	THORNO				
5750101	50 61	1 040	0.0	0.0	A A	A
R TEASAA	67854	0.1070	0.0	0.0	4.0	949
2750102	4.L=D	0.0	00			
5750200	001	510				
5750201	+0.0	478.0	0.0			
5750202	0.0	478.0	0.0			
5750203	120.0	478.0	0.0			
******	*******			********		80000000000000000
# FCCS	SYSTEM					
800390000	000000000000000000000000000000000000000					SALBASASASAS
+ FCCS PL	PING TO PC	C.	**********			
* COMPLEX	FIND IN FC					
**********	28886688888 28886688888	*********	55999393999 55999393999		********	**********
0000000	ECCSARCS		BRANCH			
6000001	0	1				
6000101	9.009-3	8.8776	0.0	0.0	-90.0	-3.2
6000102	4.0-5	0.0	00			
6000200	003	4.773856	307.22			
******	000000000000		00000000000			00000000000000
* ACCUMUL	ATOR CHECK	VALVE				
	BABERRABES	28288888888	********			
6030000	APPLIVUI V		1241 112			************
6030000	ACCHAVLY		VALVE		0.00000	
0030101	605010000	600000000	1.93221-	3 2.98310	5.48910	00000
6030201	0	0.0	0.0	0.0		
6030300	TRPVLV					
6030301	662					
***	*********	****	- 长谷谷带谷谷谷谷	****	***	****
# ACCUMUL	ATOR PIPE-	1				
*******	********	00000000000			******	*****
6050000	ACCRIPET		BRALCH			
6050001	New Irea	0	Press and Press			
6090001 4060101		0 4004			~ ~	0.0
0030101	0.014282	A . +0.27	0.0	0.0	0.0	0.0
6050102	4.0-5	0.0	00			
6050200	003	4.2190E6	307,20			
6051101	610010000	605000000	0.0	0.7	0.7	00000
6051201	0.0	0.0	0.0			
******		2.行业条件条件条件条件				5566666666666666
# ACCUMU	TOR PIPE	0				
858454481	SSABABASS.			**********		
6100000	ACCOLDES		CNGLV(1)			
6100000	ALCHIPCE		SNOLYUL .		0.0	
9100101	0.019978	1*22228	0.0	0.0	0.0	Q. V
0100105	4.0~5	0.0	00			
6100200	003	4.2190E6	307.21			
教育政府和政府的	*****	*****				
APA ACCI	UMULATOR VI	ESSEL ###				
*****	******	****				
150000	ACCUNTOR	ACCUM				
0						
*6150101	1.0905	1.8041	0.0	0.0	90.0	1.8041
P6150102	4.0E=5	0.0	10			
and the second sec	- 10 M					

#6150200 4.20E6 306.0 0.0 *6151101 610000000 0.003167 1.6 1.20 60.0 1.6 00000 0.04445 0 0 0.0 0 8 6150101 1.613734 2.33 0.0 90.0 0.0 2.33 6150102 4.0E-5 0.0 6150200 4.20E6 306.0 10 0.0 6151101 610000000 0.003167 1.6 00000 1.6 0.0 6152200 2.85 0.0 60.0 0.04445 0 0 0 **** * BWST LPIS -6200000 BWST-LP 6200101 20.44 5.0 6200102 4.0-5 0.0 TMOPVOL 0.0 0.0 90. 5.0 00 6200200 003 6200201 0.0 1.00+5 303.0 ****** * BWST HPIS 6250000 BWST-HP THOPYOL -6250101 20.44 5.0 6250102 4.0+5 0.0 0.0 0.0 90. 5.0 00 6250200 003 6250201 0.0 1.00+5 303.0 * ECC SYSTEM VALVE 6300000 ECCALVE1 VALVE 6300101 600010000 185000000 5.939-3 0.0 0.0 00100 6300201 0 .00000000 .00000000 C.0 6300300 TRPVLV 6300301 580 6310000 ECCALVE2 VALVE 6310101 600010000 180010000 5.989-3 0.0 0.0 00100 6310201 0 .00000000 .00000000 0.0 TRPVLV 6310300 6310301 580 ****** * LOW PRESSURE INJECTION SYSTEM 6350000 LPIS THOPJUN 6350101 62000000 60000000 0.0 6350200 1 615 P 185010000 0.0 6350201 -1.0 0.0 0.0 7.500 6350202 0.0 0.0 0.0 6350203 7.045 0.0 0.0 8.483+4 6350204 4.297+5 6.091 0.0 0.0 7.745+5 6350205 5.045 0.0 0.0 4.313 6350206 9.448+5 0.0 0.0 3.454 0.0 6350207 1.119+6 0.0 1.186+6 3.173 6350203 0.0 0.0
 6350209
 1.257+5
 2.673
 0.0
 0.0

 6350210
 1.326+6
 2.159
 0.0
 0.0

 6350211
 1.395+6
 1.536
 0.0
 0.0

 6350212
 1.464+6
 0.718
 0.0
 0.0

 6350213
 1.517+6
 0.000
 0.0
 0.0
 * HIGH PRESSURE INJECTION SYSTEM THOPJUN 6400000 HP15

6400101	625000000	60000000	0.0				
6400200	1	614	P	1.0010000			
6400201	-1.0	0.0	0.0	0.0			
6400202	0.0	1.58528	0.0	0.0			
6400203	0.8000+6	1.58528	0.0	0.0			
6400204	5.0000+6	1.30435	0.0	0.0			
6400205	15.060+6	0.31533	0.0	0.0			
6400205	10.000+6	0.00000	0.0	0.0			
BARRERAR .	DU.UUUTO	NON NEW YOU					
& CONTAIN	HENT	**********		SAPASEBEEBS		***********	SAMAR.
ABERBEREE	NUMBER SALAS						
R PANTATA	HENT DORVE	1 1 000 UC*	1 2 4				14688
a CUNINIA	CENT DRUKE	A LUUP MUT	LEG				
88888888888 88888888888888888888888888	**************************************	882288888888	*(0.000000000000000000000000000000000000	60.40000	×**********	0.0.0.0.0
8000000	CUNTELML		THOPVOL				
8000101 -	0.05200	0.0	3.15005	0.0	0.0	Ç. 0	
8000102	0.0	0.0	30				
8000200	003	510					
8000201	-1.0	1.00000+5	293.000				
8000202	0.0	1.00000+5	293.000				
8000203	2.0	1.24110+5	359.111				
8000204	7.0	1.55827+5	365,222				
8000205	17.7	2.36499+5	398.556				
8000206	20.	2.52357+5	400.222				
8000207	22.5	2.62700+5	401,889				
8000208	25	2.72353+6	403,000				
8000209	30.	2.81316+5	404 111				
8000210	32 5	5 8407045	104 467				
8000211	35.0	0 861/945	404.001 ADA 667				
BACADS12	22.	2 0014343	404.001				
0000212	21+2	2+0000240	404.001				
0000213	40.	2.00002+5	404.667				
8000214	42.	2.86143+5	404.657				
8000215	50.	2.83385+5	404.111				
8000216	70.	3.50000+5	404.111				
8000217	100.	3.10000+5	404.111				
8000218	150.	3.10000+5	404.111				
8000219	1.0+5	1.00000+5	293.000				
**	***********	****	1444404044	10000000000000	****	******	00000
· CONTAIL	NMENT BROKE	EN LOOP COL	D LEG				
****	******	*****	****	*********	*****	848666666666	64440
8050000	CONTALHL		TMDPVOL				
8050101	0.05200	0.0	4.08155	0.0	0.0	0.0	
8050102	0.0	0.0	00				
8050200	003	510					
8050201	-1.0	1-00000+	5 293.000				
8050202	0.0	1.00000+	5 293,000				
8050203	2.0	1.24110+	5 359,111				
8050204	7.0	1 55807-	5 365 333				
8050205	17 7	3 364004	2 202 4 C C C				
0050200	11+1	0 60067.	2 270.220				
0020200	20.0	2.0262214	2 400.222				
0050201	22.03	2.02/00+	5 401.887				
8050208	20.	2.12353+	5 403.000				
8050209	30.	2.81316+	5 404.111				
8050210	32.5	2.84074+	5 404.667				
8050211	35.	2.86143+	5 404.667				
8050212	37.5	2.86832+	5 404.667				
8050213	40.	2.86832+	5 404.667				
8050214	45.	2.86143+	5 404,667				
8050215	50.	2.83385+	5 404.111				
8050216	70.	3.50000+	5 404,111				
8050217	100-	3,10000+	5 404-111				
8050218	150.	3.10000+	5 404 111				
8050219	1.0+5	1.00000+	5 293,000				
* CONTAINMENT POWER OPERATED PELIEF VALVE ****** 8100000 CONTPORV THOPVOL 0.0 8100101 0.0 0.1 0.0 0.0 1.0 8100102 0.0 0.0 00 8100200 003 510 1.00000+5 293.000 8100201 -1.0 1.00000+5 293.000 8100202 0.0 1.00000+5 293.000 8100203 1000.0 * BOUNDARY VALVE INTACT LOOP HOT LEG *9000000 BDUNDVLV VALVE *9000101 420010000 905000000 0.0 0.0 0.0 00100 0 0.0 #9000201 0.0 0.0 TRPVLV *9000300 +9000301 501 * BOUNDARY VOLUME INTACT LOOP HOT LEG 特别的行为保障部分的保障部分的保障部分的保存的保存的保存的保障部分的保障部分的保存的存在的存在分子的保障部分的不合义。 THOPVOL *9050000 BOUNDVOL *9050101 0.0 1.0 0.1 0.0 0.0 0.0 *9050102 0.0 0.0 00 #9050200 001 614.88 1.0 #9050201 0.0 614.88 *9050202 1000.0 * BOUNDARY JUNCTION FOR PREZ WATER LEVEL \$ *9100000 BDUNDTJ THOPJUN *9100101 915000000 415000000 0.0 #9100200 1 CNTRLVAR 100 501 *9100201 -10.0 *9100202 -10.0 0.0 0.0 0.0 -500.0 0.0 0.0 #9100203 0.0 0.0 0.0 0.0 *9100204 10.0 0.0 500.0 0.0 ***** * BOUNDARY VOLUME FOR PREZ WATER LEVEL *9150000 BOUNDTY IMDPVOL 1.0 *9150101 0.0 0.0 0.0 0.0 0.1 0.0 00 #9150102 0.0 501 TEMPE *9150200 001 415010000 +9150201 -0.0 0.0 613.55 *9150202 0.0 0.0 0.0 *9150203 700.0 0.0 700.0 * REACTOR VESSEL HEAT STRUCTURE * REACTOR VESSEL WALL HEAT STRUCTURES ****** * REACTOR VESSEL FILLER BLOCKS HEAT STRUCTURES *** * INLET ANNULUS TOP VOLUME 1 * STATION 264 TO 2 77 12000000 1 21 1 0.508 2 12000100 0 20 12000101 0.7264 4 12000201 20 12000301 0.0 20

12000401 12000 1 12000601 12000701 12000801	559.75 200010000 0 0	21 0 0.0 0.1524	1 0 0.0 0.3245	1 1 0.0 0.33	0.165 0.165 1 1	1
* INLET AN * STATION	INULUS TOP 264 TO 2	VOLUME 2	5 ÷ ÷ * > : * * * ÷ ÷ ÷ ÷	69999008009		00000000000000000000000000000000000000
				**********		00000000000000
12001000 12001100 12001201 12001201 12001301	1 20 4 0.0 559 77	21 2 0.7264 20 20	2	1	0,508	
10000000	********	6 m				
12001201	590010000	0	1	1	0.162	1
15001001	0	0	0	1	0.165	1
12001701	0	0.0	0.0	0.0	1	
12001801	0	0.1524	0.3245	0.33	1	
*****		*****	*******	*****		*******
* INLET AN * STATION	NULUS LOWE 247.3 TO	ER VOLUME 1 264.0				
*****	(你你你你你你你你你?	合金的最大教会会会 经	6 位益部公益计量存益。	各部合作的部分合作	各部的教育教育教育	白教会会会会会会会会会会会
12020000 12020100 12020101	1 0 20	21 1 0.7264	2	1	0.501	
12020201	4	20				
TENTOTOT	227,00	61	- 20 C C C C C C C C C C C C C C C C C C	1.00		
15050001	202010000	0	1	1	0*575	1
12020601	0	0	0	1	0.212	1
12020701	0	0.0	0.0	0.0	1	
12020801	0	0.1524	0.3245	0.424	1	
******						88898888888888888
* INLET AN * STATION	NULUS LOWE 247.3 TO	ER VOLUME 2 264.0	-			
****		******		****	******	400000000000000
12021000	1	21	2	1	0.501	
12021100	õ	1				
12021101	20	0-7264				
12021201	4	20				
10001201	~ ~	20				
+=061001	0.80	20				
TENETANT	229.12	62	and the second			
15051501	282010000	0	1	1	0.212	1
12021601	0	0	0	1	0.212	1
12021701	0	0.0	0.0	0.0	1	
12021801	0	0.1524	0.3245	0.424	1	
*******	****	*********	000000000000		1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	*****
* DOWNCOME	R 1 AND LC	W PLENUM				
. STATION	67.7 TO	247.3				
*******			00000000000			*********
12100000	6	21	2	1	0.47	
12100100	~	1	.6.	*		
12100101	20	0 7044				
10100001	20	011200				
72700501	4	20				
12100301	0.0	20				
12100401	545.0	21				
12100501	204010000	2000000	1	1	0.479	4
12100502	215010000	0	1	1	0.36	5
12100503	220010000	0	1	1	0.37	6
12100601	-939	0	3949	1	0.470	4
12100602	-930	0	3949	1	0.36	5

12100603	-939	0	3949	1	0.37	6
12100701	0	0.0	0.0	0.0	6	
12100801	0	0.1015	0.2100	0.958	4 5	
12100802	0	0.1016	0.2155	5.00	6	
6000566900 ********				*****	******	000000000000000
. DOWNCOME	R 2					
*******	********		0000000000	**********	****	404404044
12101000	4	21	2	1	0.47	
12101100	0	1 7364				
12:01201	20	20				
12101301	0.0	20				
12101401	545.0	21				
12101501	284010000	2000000	1	1	0.479	4
12101601	-939	0	3949	1	0.479	4
12101701	0	0.0	0.0	0.0	6	
12101801	0	0.1010	U.E152	5488.800 . U		******
* CORE SU	PRURT BARRI	EL (SECTIO	0 1)			
* STATION	96.44 TO	277				
********	*******	********		********	********	******
12150000	6	11	2	1	0.381	
12150100	0	1				
12150101	10	0.419				
12150301	0.0	10				
12150401	559.60	11				
12150501	0	0	0	1	0.165	1
12150502	0	0	0	1	0.212	2
12150503	0	0	0	1	0.479	6
12150601	200010000	0	1	1	0.165	1
12150602	202010000	2000000	-	1	0.479	6
12150701	0	0.0	č.0	0.0	6	×
12150901	õ	0.1016	0.2155	0.330	1	
12150902	0	0.1016	0.2155	0.424	2	
12150903	0	0.1016	0.2155	0.958	6	
	10000x 0400	「ひかかかかなないなる	· · · · · · · · · · · · · · · · · · ·	0 6 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9	4555555555555	***********
& STATION	PORT DARN	277	14 61			
*****	*****			*********	*****	********
12151000	0	11	2	1	0.381	
12151100	0	1				
12151101	10	0.419				
12151201	4	10				
12151401	540 45	11				
12151501	0	õ	0	1	0.165	1
12151502	0	0	ò	ī	0.212	2
12151503	0	0	0	1	0.479	6
12151601	280010000	0 0	1	1	0.165	1
12151602	282010000	0 0	1	1	0.212	2
12151603	284010000	0 2000000	1	1	0.417	0
12151901	0	0.1016	0.2155	0.330	1	
12151902	Ö	0,1016	0.2155	0.424	2	
12151903	0	0.1016	0.2155	0.958	6	
*****	*****	****	****	*********	*******	************************
* FLOW S	KIRT - COR	E FILLER	ASSEMBLY			
A STATIC	N 96.44 TO	261.13				500000.00.00000000
P 12 12 12 12 12 13 14 15	0 1 0 2 0 0 0 0 0 0 0	AN 14 18 1. 18 18 18 13 13 18 18			ALC: NO 10 10 10 10 10 10 10 10 10	the set of the set of the ball of the set of the ball the set

12250000	10	5	2		0.3	
12250100	0	1				
12250101	4	0.38				
12250201	4	4				
12220201	0.0	4 E				
10050501	225010000	0			0 5000	
12250502	227010000	1000000	1	1	0.2795	4
12250503	232010000	0	1	1	0.3775	7
12250504	240010000	5000000	1	ĩ	0.5590	9
12250505	250010000	0	1	1	0.8430	10
12250601	0	0	0	1	0.5200	1
12250602	0	0	0	1	0.2795	6
12250603	0	0	ç	1	0,3775	7
12250604	0	0	0	1	0.5590	9
12250000	0	0 0	2.0	1	0.5420	10
12250801	0	0.6	5.0	0.520	1	
12250802	ŏ	0.6	ŏ.ŏ	0.2795	Ĝ	
12250803	0	0.6	0.0	0.3775	7	
12230804	0	0.6	0.0	0.5590	9	
12250005	0	0.6	0.0	0.8430	10	
***	● ● ● ● ● ● ● ● ● ● ● ● ● ● ● ● ● ● ●	2. 教育教育教育教育教育	60000000000000000000000000000000000000	********		*****
> LOWER CO	IRE SUPPORT	STRUCTURE				
* STATION	96.44 TO	116.91			OPT	
+ INCLUDES	CORE SUPP	ORT BARREL	LIPYLOWER	R CORE SUPP	ORI	
* 5100L100	LE AND FUEL	SAABAAAAAA	INCH CHU S	СЦАСЭ Хабалальная		
12251000	1	7	2	1	0.282	
12251100	ō	1		~		
12251101	6	0.3				
12251201	4	6				
12251301	0.0	6				
12251401	559.64	7				
12251501	225010000	0	1	1	0.52	1
12251701	0	0.0	0 0	0 0	1	+
12251801	0	0.095	0.095	0.52	ĩ	
***		******	******			****
* ACTIVE	CORE					
. STATION	116.91 70	182.94				
***	*****	*****	· 公 む 谷 む 谷 む む む む む む む む む む む む む む む	****	199999999999999 199999999999999	00400444 · 04
* AVERAGE	FUEL RODS	S IN AVERAC	SE CHANNEL	CAXIAL LEVE	L 1)	
**************************************	·************	100000000000000000000000000000000000000	10080000000000 7	1 1	0.0	186989996688 8 4
*	-	1	2 8	*	0.0	
12361100	õ	î				
12361101	5	4.66893-3				
12361102	1	4.74351-3				
12361103	3	5.36265-3				
12361201	1	5				
12361202	-2	0				
12361203	1.0	5				
12361302	0.0	9				
12361401	1080.3	1				
12361402	1065.4	2				
12361403	1022.3	3				
12361404	954.05	4				
12361405	864.85	2				
12361405	616 50	7				
2 4 3 1 L M U I	0.40.4.2.4					

12361408 12361409 12361410 12361501	610.30 604.29 598.48 0	8 9 10 0	0	1	306.222	1
12361601 12361701 12361901	227010000 900 0	0.127545 0.013633	0.0	1 0.0 0.2795	306.222 1 1	1
* AVERAGE	FUEL RODS	S IN AVERAS	SE CHANNEL	CAXIAL LEV	EL 20	
* 12362100 12362100 12362101 12362102 12362102 12362202 12362202 12362202 12362301 12362402 12362403 12362404 12362405 12362405 12362405 12362407 12362407 12362409 12362409 12362409 12362401 12362409 12362409 12362401	1 1 0 5 1 3 1 -2 -3 1.0 0.0 1402.1 1374.5 1168.5 1005.1 826.87 644.72 635.29 626.18 617.36 0 228010000	10 1 4.68060-3 4.74415-3 5.6341-3 5.6341-3 5.69 5.9 12345-67 8910 000	2 8	1	0.0 306.222 306.222	1
12362701	900	0.197174 0.013633	0.0	0.0	1	
* AVERAGE	FUEL ROD	S IN AVERA	GE CHANNEL	CAXIAL LEV	EL 3)	
<pre>* 12363000 * 12363100 12363100 12363102 12363102 12363202 12363202 12363202 12363202 12363401 12363402 12363403 12363404 12363405 12363405 12363406 12363407 12363407 12363409 12363409 12363409</pre>	1 1 0 5 1 3 1 2 3 0 4 2 3 0 4 4 2 3 1 0 4 4 2 2 3 0 4 4 2 2 3 0 4 4 2 2 3 0 4 4 2 2 3 1 2 4 - 2 - - - - - - - - - - - - -	10 1 4 * 68112-3 4 * 74424-3 5 * 36350-3 5 6 9 5 9 5 9 1 2 3 4 5 6 7 8 9 10 0 0 0 0 0 0 0 0 0 0 0 0 0	2 8	1	0.0	
12363601	229010000	0.201827	1.0.0	1	306.222	1

12363901	0	0.013633	0.0	0.2795	1	
AVERAGE	FUEL RODS	IN AVERAG	E CHANNEL (AXIAL LEVE	L 4)	
12364000 + 12364100 12364101 12364102 12364202 12364202 12364203 12364203 12364301 12364302 12364401 12364403 12364405 123645 123645 123656 123656 123656 123656 12365656 12365656 12365656565656565656565656565656565656565	1 1 0 5 1 3 1 -3 1.0 0.0 1199.4 1180.4 109.4 1180.5 10.0 10	10 1 4 • 67304-3 4 • 74412-3 5 • 36335-3 5 • 5 9 5 9 1 2 3 4 5 • 6 7 8 9	2 8	1	0.0	
12364410 12364501 12364601 12364701 12364901	617.38 0 230010000 900 0	10 0 0.150138 0.013633	0 1 0.0 0.0	1 0.0 0.2795	306.222 1 306.222 1 1 1	
* 12365000 + 12365100 12365101 12365102 12365103 12365201 12365203 12365203 12365203 12365203 12365301 12365302 12365401 12365403 12365404 12365405 12365406 12365406 12365409 12365409 12365401 12365501 12365701 12365701	1 1 0 5 1 -2 -3 1.0 0.0 920.10 920.10 911.62 886.56 845.91 791.96 726.87 623.37 619.27 615.33 611.53 0 231010000 900 0	10 1 4.66378-3 4.74379-3 5.36299-3 5 9 5 9 1 2 3 4 5 6 7 8 9 10 0 0 0.084338 0.013633	2 8 0 1 0.0 0.0	1 1 1 0.0 0.2795	0.0 306.222 1 306.222 1	
* AVERAGE	FUEL ROD	S IN AVERA	GE CHANNEL	(AXIAL LEVE	0.0	
1000000	4	1	0			

12366100 12366102 12366103 12366202 12366203 12366203 12366302 12366302 12366401 12366403 12366403 12366403 12366405 12366405 12366405 12366407 12366409 12366409 12366409 12366601 12366501	0 5 1 3 1 -2 -3 1.0 0.0 665.18 663.63 655.33 655.33 655.33 655.33 655.33 655.33 655.33 655.53 657.34 599.70 597.74 599.70 597.74 597.74 596.81 0 232010000 900 0	1 4.65917-3 4.74339-3 5.36250-3 5 9 1 2 3 4 5 6 9 1 2 3 4 5 6 9 1 0 0 0.020229 0.013633	0.1.0	1 1 0.0 0.2795	306.222 306.222 1	1
# AVERAGE	FUEL RODS	S IN HOT (CHAN' EL	(AXIAL	LEVEL 1)	
12371000 12371100 12371101	1 0 5	10 1 1 4.67914-3	2 8	1	0.0	
12371102 12371201 12371202 12371203 12371203 12371301 12371302 12371401 12371402 12371404 12371404 12371404 12371405 12371406 12371406 12371407 12371408 12371409 12371409 12371400 12371400 12371400 12371501 12371501 12371601 12371901 *	1 3 1 -2 -3 1.0 0.0 1396.3 1369.4 1291.0 1167.7 1007.5 832.22 643.06 633.82 624.88 616.24 0 233010000 900 0 EUEL BOD	4.74659-3 5.36552-3 5 9 5 9 1 2 3 4 5 6 7 8 9 10 0 0 3.45563-2 0.013633 5 10 H0T	0 1 0.0 0.0	1 1 0.0 0.2795	54.7624 54.7624 1	
* AVERAGE	FUEL ROD	S IN HOT	CHANNEL	(AXIAL	LEVEL 2)	
12372000 + 12372100 12372101 12372102 12372103	1 0 5 1 3	10 1 4.69746-3 4.74708-3 5.36610-3	8	1	0.0	
12372201 12372202	1_2	5				

ġ

12372203 12372301 12372401 12372402 12372402 12372403 12372404 12372405 12372405 12372405 12372405 12372405 12372405 12372405 12372405 12372405 12372405 12372405 12372405 12372405	-3 1.0 0.0 1855.5 1807.9 1667.1 1444.1 1165.5 870.55 661.11 647.03 633.36 620.08 0 234010000 900 0	9 9 9 9 9 9 9 12 3 4 5 6 7 8 9 10 0 5 9 10 0 5 9 10 0 5 9 10 0 5 9 10 0 5 9 10 0 5 9 10 0 5 10 0 5 10 0 5 10 0 5 10 0 5 10 0 5 5 5 5	0100	1 1 0.0 0.2795	54.7624 54.7624 1	1
* AVERAGE	FUEL RODS	S IN HOT	CHAMIEL	(AXIAL	LEVEL 3)	
* 12373000 + 12373100 12373101 12373102 12373202 12373202 12373203 12373203 12373203 12373401 12373401 12373403 12373404 12373405 12373406 12373406 12373407 12373407 12373407 12373409 12373501 12373501 12373601 12373901	1 1 0 5 1 -2 -3 1.0 0.0 1861.3 1813.5 1672.0 1447.8 1167.7 871.21 661.84 647.72 634.01 620.70 0 235010000 900 0	10 1 4.69770-3 4.74714-3 5.36616-3 5 9 5 9 1 2 3 4 5 6 7 8 9 10 0 5.35414-2 0.013633	2 8 0 1 0.0	1 1 0.0 0.2795	0.0 54.7624 54.7624 1	1
* AVERAGE	FUEL RODS	S IN HOT	CHANNEL	CAXIAL	LEVEL 4)	
* 12374000 * 12374100 12374101 12374102 12374201 12374202 12374202 12374203 12374301 12374301 12374401 12374401	1 1 0 5 1 3 1 -2 -3 1.0 0.0 1504.5 1472.8 1380.4	10 1 4.68411-3 4.74696-3 5.36594-3 5 9 5 9 1 2 3	2	1	0.0	

12374404 12374405 12374406 12374407 12374409 12374409 12374409 12374501 12374501 12374601 12374701	1234.8 1049.2 846.83 650.05 639.69 629.67 619.95 0 236010000 900 0	4 5 6 7 8 9 10 0 0 3.89479-2 0.013633	01.0	1 1 0.0 0.2795	54.7624 54.7624 1	1
* AVERAGE	FUEL RODS	14 HOT	CHATINEL	(AXIAL	LEVEL 5)	
12375000 12375100 12375100 12375102 12375103 12375201 12375202 12375203 12375203 12375301 12375402 12375403 12375405 12375405 12375406 12375406 12375408 12375409 12375409 12375409	1 1 0 5 1 3 1 -2 -3 1.0 0.094.0 1079.3 1036.4 8 1.49 0.094.4 8 1.49 778.20 635.57 629.61 623.86 618.32	10 1 4.66963-3 4.74674-3 5.36570-3 5 6 9 5 9 1 2 3 4 5 6 7 8 9 1 0 1 1 1 1 1 1 1 1 1 1 1 1 1	28	1	0.0	
12375501 12375601 12375701 12375901	0 237010000 900 0	0 2.21880-2 0.013633	0 1 0.0 0.0	1 0.0 0.2795	54.7624 54.7624 1 1	1
AVERAGE	FUEL ROD	S IN HOT	CHANNEL	(AXIAL	LEVEL 6)	
12376000 + 12376100 12376101 12376102 12376201 12376202 12376203 12376203 12376301 12376301 12376401 12376401 12376403 12376405 12376406 12376406 12376407 12376408 12376409	1 1 0 5 1 -2 -3 1.0 0.0 750.24 737.27 721.29 671.37 620.33 616.67	10 1 4.66100-3 4.74638-3 5.36527-3 5 6 9 5 9 1 2 3 4 5 6 7 8 9	2	1	0.0	

12376410 12376501 12376601 12376701 12376901	614.94 0 238010000 900 0	10 0 0.68731-2 0.013633	0.0	1 0.0 0.2795	54.7624 54.7624 1 1	1
· HOT	FUEL RODS	S IN HOT	CHANNEL	(AX]AL	LEVEL 1)	
* 12381000 * 12381100 12381101 12381102 12381201 12381202 12381202 12381202 12381203 12381203 12381401 12381403 12381405 12381405 12381405 12381407 12381409 12381409 12381401 12381501 12381501 12381701	1 1 0 5 1 3 1 -2 -3 1.0 0.0 1501.4 1470.3 1379.6 1236.6 1053.9 854.07 646.82 636.62 636.62 626.75 617.18 0 233010000 900	10 1	28	1	0.0 2.23520 2.23520 1	11
	FUEL DOD	e 11 Unt	e la unite	V.213		
* HUI *	FUEL RUD	o in Hui	Chiner	CANIAL	LEVEL 27	
12382000 + 12382100 12382101 12382102 12382202 12382202 12382202 12382202 12382202 12382401 12382402 12382402 12382405 1238245 1238245 1238245 1238245 1238245 1238245 1238245 1238245 1	1 1 0 5 1 3 1 - 3 1 - 3 0 - - - - - - - - - - - - -	10 1 4.69746-0 4.74.08-3 5.76613-3 5 9 12 3 4 5 6 7 8 9 10	2 8	1	0.0	
12°92501 12582601 12382701 12382901	0 234010000 900 0	0 2.37504~1 0.013633	0 0.0 0.0	1 0.0 0.2795	2.23520 2.23520 1 1	1

P

ø	HOT	FUEL	RODS	IN HOT	CHANNEL	(AXIAL	LEVEL 3)	
*		96 - S S						
1238	3000	1		10	2	1	0.0	
*		1		1	6			
1230	3700	0						
1230	2101	2		4.69110-3				
1238	2102	1	1. T	4.74714=3				
1230	3202	3		5.30516-3				
1238	2201	1		2				
1630	2202	-2		0				
1220	3202	-2		9				
1222	2201	1+0		2				
1220	2226	0.0		7				
1030	2/00	ZUUZAL 1040 A		-				
1332	3403	1700 5		3				
1233	3454	1560 0		2				
124:	3405	1005 0		5				
1231	13404	LCC EL		6 6				
1233	3407	665 6		7				
1231	13408	650.33	5	A				
123	13409	635.41	2	9				
123	83410	621.06	<u>.</u>	10				
123	83501	0		0	0	1	2.23520	1
123	63601	235010	0000	0	1	1	2.23520	1
123	83701	900		2.37012-3	0.0	0.0	1	
123	83901	0		0.013633	0.0	0.2795	1	
4								
÷	HOT	FUEL	RODS	IN HOT	CHANNEL	CAXIAL	LEVEL 4)	
\$								
123	84000	1		10	2	1	0.0	
*	1.1.1.1.1.1	1		1	8			
123	84100	0		1				
123	84101	5		4.68411-3				
123	84102	1		4.74696=3				
123	84103	3		5.36594-3				
123	84201	1		2				
123	84202	-2		0				
123	84200	-3		9				
100	04303	1.0		0				
100	04202	1803		1				
101	64403	1557	7	1				
123	84403	1454	4	2				
123	84404	1201	a	4				
123	84405	1086.	8	5				
123	84406	863.2	a	6				
123	84407	652.6	6	7				
123	84408	641.5	1	8				
123	84409	630.7	1	9				
123	84410	620.2	3	10				
123	84501	0		0	0	1	2.23520	1
123	84601	23601	0000	0	1	ī	2.23520	1
123	84701	900		1.71484-	3 0.0	0.0	1	
123	84901	0		0.013633	0.0	C.2795	1	
\$2								
* +	INT FUE	L ROD	TN H	JT CHANNEL	CAXIAL LE	VEL5)		
\$						1.5.5.1.1.1.2		
123	185000	1		10	2	1	0.0	
+		1		1	8			
12:	001238	0		1				
121	385101	5		4.66963-	3			

12385102 12385203 12385202 12385203 12385203 12385302 12385302 12385402 12385403 12385403 12385405 12385405 12385406 12385406 12385406 12385406 12385409 12385409 12385409 12385501 12385501 12385501	1 3 1 -2 -3 1.0 0.0 1139.7 1123.5 1075.6 1000.7 903.61 790.08 637.14 630.72 624.53 618.55 0 237010000 900 0	4.74674-3 5.36570-3 5 9 5 9 1 2 3 4 5 6 7 8 5 10 0 0 9 10 0 0 9 10 0 0 9 10 0 0 0.97663-3 0.013633	010.0	1 1 0.0 0.2795	2.23520 2.23520 1	1
* HOT FUE	L ROD IN HO	T CHANNEL	(AXIAL LE	VEL 6)		
12386000		10	2			
•	ĩ	1	8	*	0.0	
12386100	0	1				
12306101	5	4,66100-3				
10306102	1	4.14638=3				
10306200	2	2.20227=3				
75300501	7	2				
12300202	-2	6				
12360203	-3	9				
12386301	1.0	5				
12386302	0.0	9				
12386401	771.60	1				
12386402	767.79	2				
12386403	756.45	3				
12386404	737.83	4				
12386405	712.35	5				
12386406	680.55	6				
12386407	621.74	7				
12386408	619.61	8				
12386409	617.56	9				
12386410	615.58	10				
12386501	0	0	0	4	2 23520	
12386601	23:010000	0	1	1	2 23520	1
12386701	900	0.32091-3	0.0	0.0	1	1
12386901	0	0.013633	0.0	0.0705	-	
	*********	5655666538	NEESSERE.	V.22190		
* UPPER C	DRE SUPPOR	T STRUCTUR		*********	8884588885	88888888888888888888888888888888888888
# STATION	190.5 TO	234.5	-			
*****	*********	6666668888				
12400000	2	7	2	4 282849	0393399979999	**********
12400100	õ		6	+	0.282	
12400101	6	0.31				
12400201	4	6				
12400301	0.0	6				
12400401	500 40	7				
12400501	240010000	E000000		- 1997 - N. S. S.		
12400401	240010000	0000000	1	1	0.559	2
12400701	0	0	0	1	0.559	2
A A A A A A A A A A A A A A A A A A A	- M2	Usu	0.0	0.0	2	

12400801 (0	0.56	0.0	1.118	2	
· · · · · · · · · · · · · · · · · · ·	0 \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	*******	****	****	*****	****
* FUEL MODI	JLES					
* STATION :	187.6 TO 2	58.4				
*****	*****	******	*****	有些教教教教会的教育	*****	你你你你你你你你你你你你
12510000	1	5	1	1	0.0	
12510100	0	1				
12510101	4	0.01				
12510201	4	4				
12510301	0.0	4				
12510401	592.73	5				
12510501	250010000	0	4. T. A. T. M. A.		1 2	
12510601	251010000	0	-	*	1 0	
12510701	551010000	0.0	÷ •	*	4.2	*
12510201	0	0.0	0.0	0.0	*	
12510001	0	0.0	0.0	1.0	*	
ACJIU701		0.0	VeV	7.0	*	
	REFERENCESSER	**********	008008000000		*******	,当会计会会会经行会会会会
NUPPER PLE	NUM INTERN	ALS				
88888888888888888888888888888888888888	\$\$\$\$\$\$\$\$\$\$\$	- - 	**********	2. 你 你 你 你 你 你 你 你 你 你 你 你 你 你 你 你 你 你 你	*****	1-2-2-2-2-2-2-2-2-2-2-2-2-2-2-2-2-2-2-2
12551000	2	5	1	1	0.0	
12551100	0	1				
12551101	4	0.005				
12551201	4	4				
12551301	0.0	4				
12551401	590.62	5				
12,551501	255010000	0	1	1	1.0	2
12551601	0	0	0	ĩ	1.0	3
12551701	0	0.0	0.0	0.0	2	
12551801	0	0.0	0.0	1.0	2	
*****			00000000000			
A CURE SUP	PORT BARRE	I - UPPER	PLENUM LOW	FR VOLUME		*************
* STATION	264 TO 297	1.6		nen voeone		
*********	ABERAABERA	LBGSSSSSSS				
12552000	1	11	9 9	4	A 201	********
12552100	2		6	+	0.597	
19650101	10	0.110				
10550001	10	0.0013				
10550001	2	10				
1955914901	0.0	10				
10250501	370.62	11				
10550/01	232010000	0	1	1	0.854	1
12002001	0	0	0	1	0.859	1
12552701	0	0.0	0.0	0.0	1	
12352801	0	0.762	0.0	0.854	1	
****	5 & & & & & & & & & & & & & & & & & & &	****	设备条款价格的条款价	*****	****	****
* CORE SUP	PORT BARRI	EL - UPPER	PLENUM TO	P VOLUME		
* STATION	297.6 TO :	325				
發展 经收益 化合金	56600000000000	***	040#30#600	***	********	*****
12601000	1	21	2	1	0.381	
12601100	0	1				
12601101	20	0.728				
12601201	5	20				
12601301	0.0	20				
12601401	590.62	21				
12601501	255010000	0	1	1	0.712	
12601601	0	0	5	1	0.710	4
12601701	0	0.0	0.0	0.0	1	
12601801	0	0.762	0.0	0 210	4	
******	C B B B B B B B B B B B B B B B B B B B	BBBBBBBBBBB	NARABARA	Vell2		
& LIPPER L	FAD TOP DI	ATE	**********	********	*********	(1) 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
& STATION	325					
& BAABAAAAA	263					
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12602201	5	20				
12602301	0.0	20				
11602401	575.50	21				
12602501	255010000	0	1	1	0.712	*
12602601	-939	0	3949	1	0.712	:
12602701	0	0.0	0.0	0.0	1	*
12602801	0	0.0	0.0	0.712	1	
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10060000	8	8	2	1	0.0051054	
10060100	0	1			0.00024054	
10060101	7	6.348984-3				
10060201	6	7				
10060301	0.0	7				
10060401	559.65	1				
10060402	558.37	2				
10060403	557.09	3				
10060404	556.16	4				
10060405	555.12	5				
10060406	553.83	6				
10060407	552.68	7				
10060408	551.56	8				
10060501	115010000	10000	1	1	1124.71	3
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10060701	0	0.0	0.0	0.0	8	
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* SHROUD	- UPPER SEC	CTION -1.0				
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15000000	2	4	2	1	0.3048	
15000100	0	1				
15000101	3	0.3143				
15000201	5	3				
15000301	0.0	3				
15000401	546.76	4				
15000501	515060000	0	1	0	1.58726	1
15000502	515050000	0	1	1	0.92736	2
15000601	505010000	0	1	0	1.63672	1
15000602	507010000	0	1	1	0.92736	2
15000701	0	0.0	0.0	0.0	2	
15000801	0	0.0	0.0	0.0	5	
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15100000	4	4	2	1	0.6445	
15100100	0	1				
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15100301	0.0	3					
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10100006 -	212030000	-10000	1	0		2.46800	4
12100601	508010000	0	1	1		0.646354	1
15100602	510010000	10000	1	0		2.51723	4
15100701	0	0.0	0.0	0.	0	4	
15100801	0	0.0	0.0	0.	0	4	
15100901	0	0.0	0.0	0	0	2 · · · · · · · · · ·	
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20100300	TBL/FC N-	1	1	40	ZR		
20100400	TBL/FCTN-	1	1	4	S-STELL		
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20100600	TEL /FCTN	4	A	12	INCOMPANY	600	
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20100110	1.36648E3	2.713792					
20100111	1.5331553	2.521600					
20100112	1 2121023	2 446000					
20100113	1.0000000	2.440790					
20100115	T*04495ED	2,371073					
20100114	1.9775953	2.289762					
20100115	2.2553783	2.307069					
20100116	2.53315E3	2.433413					
20100117	2.81093E3	2.661870					
20100118	3-0887153	2,994171					
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20100155	1.37315E3	3.4438445	6				
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20100103	2.0701023	4.002412E	5				
20100190	2.67315E3	0.C15829E	6.00				
20100161	2.77315E3	6.320980E	6				
20100162	2.87315E3	6.582538F	6				
20100163	2.9731553	6.7133175	6				
20100164	3-1131553	6.8005035	6				
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20100203	810.0	0.29
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20100302	380.4	13.6
20100303	469.3	14.6
20100304	577 6	15.8
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20100305	665.9	17.5
20100306	774.8	18.4
20100307	872.0	19.8
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50100304	10/3+2	23.2
20100310	1123.2	25.4
20100311	1152.3	24.2
20100312	1232.2	25.5
20100070	122686	
2010003:2	7537*4	20+0
20100314	1404.2	28.2
20100315	1576.2	33.0
20100316	1625.2	36-7
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20100353 20100354 201 0355 20100356 20100357 20100358 20100359 20100360	300.0 400.0 1090.0 1093.0 1113.0 1133.0 1153.0 1173.0 1193.0	1.841E6 1.978+6 2.168E6 2.456E6 3.288E6 3.865E6 4.028E6 4.028E6 5.345E6 5.044E6
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20100353 20100354 201 0355 20100356 20100357 20100358 20100359 20100360 20100361 20100362	300.0 400.0 1090.0 1093.0 1113.0 1133.0 1153.0 1173.0 1193.0 1213.0	1.841E6 1.978+6 2.168E6 2.456E6 3.288E6 3.865E6 4.028E6 4.709E6 5.345E6 5.044E6 4.054E6 3.072E6
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20100353 20100354 20100354 20100356 20100357 20100358 20100359 20100360 20100361 20100362 20100363 20100364	300.0 400.0 640.0 1090.0 113.0 113.0 1153.0 1153.0 1173.0 1193.0 1213.0 1233.0 1243.0 3000.0	1.841E6 1.978+6 2.168E6 2.456E6 3.288E6 3.865E6 4.028E6 4.028E6 5.345E6 5.044E6 4.054E6 3.072E6 2.332E6 2.332E6
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20100602	477.5	15.92	
20100603	588.7	18.17	
20100604	700.0	20.42	
20100605	810.0	22,50	
20100606	655.0	94.65	
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20100731 3	373.15	2033.52				
20100752	422.04	2004.59				
20100753	477.59	1971.74				
20100754	533.15	1938.87				
20100755	585.71	1906.01				
20100756	644.26	1873.15				
20100757	699.82	1840.29				
20100758	755.37	1877.43				
20100759.	810.93	1774.56				
20100760	866.48	1741.70				
20100761	922.04	1708.84				
20100762	917.59	1072:96				
20100763	10715	1042.11				
20100784	1088.71	1510.25				
20100762	1100 00	1011407				
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20100748	1010.03	1478,80				
20100769	3366 48	1645.94				
20100770	1422.04	1413.08				
20100771	1477.50	1380.22				
20100772	1533.15	1347.35				
20100773	1588.71	1314.49				
20100774	1644.26	1281.63				
20100775	1699.82	1245.77				
20100776	1755.37	1215.90				
20100777	1810.93	1183.04				
20100778	1866.48	1150.18				
20100779	1922.04	1117.32				
20100780	5000.00	1117.32				. Carner
****	04444448644	095090-1888	80000000000000000000000000000000000000	000000000000000000000000000000000000000	5888888888866600883	498568
* NICHRUM	E . THERMA	F. CONCIDENT	VIII			LINANS
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. NICHROM	E - VOLUME	TRIC HEAT	CAPACITY			
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20100851	373.15	2180.80				
20100852	1922.04	2160.80				
20100853	5000.00	2180.80				1.1.1.1
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* GENERAL	TABLE DAT	4				Section Section
******	*********	******	******	自己移动的复数形式动力的	*****	5449999 9
* TABLE						
. NUMBER	DESC	RIPTION #1				
8 ======	DEAC	TOU DOUTD	VE TIME	AFTER CODAM		
* 900	RCAL	TUR FUNER	VD4 IIME	AFIER SCRAD		0000000
20.00000	DRUED	510	1.0	36.0+6		12-5
20290001	0.0	1.0		2010-010		
20290002	0.1	0,9004.0		# FR0: 12	-3 POSTTEST	
20290003	0.2	0.274300				
20290004	0.3	0.153171				
20290005	0.4	0.110821				
20290006	0.5	0.091625				
20290007	0.6	0.083212				

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ai 1111

20290008	0.8	0.073556																		
0000000	1.0	0.064999																		
CONADORA	1+0	040-4111																		
20290010	1.5	0.0.3089																		
20290011	2.0	0.059854																		
565679944	5.0	A 489328																		
20240015	3+0	0.021202																		
20290013	4.0	0.055204																		
41000000	6.0	0.052085																		
EVE VVVV	0.0	A ALASSI																		
20290015	0 = 0	0+047176																		
20200016	10.0	0.047947																		
20203017	15 0	D. C. LEVE																		
ENCARNTI	7446	44 . 4212																		
20290018	20.0	0:0+2178																		
20290019	30.0	0.038783																		
55557VV87	10.0	A 6313.3																		
RARADORA	40.0	0.020248																		
20290021	60.0	0.031546	5																	
200000022	1.46	0.001440	A F	0.5	st 1	4.5	- 1	1200	32	-1	3.00	173								
RVETULES.		1 494240		10.57		1.17		6.4.5	83			8 C 10								
	**********	2	14000	8.0	8.8.1	44	8.81	0.0.0	8.9	0.6	9.9	2.0.6	8.97	4.4	6.6.1	5.6.1	5.05.4	9.9.9	0.0.01	2.0.0
# ENVIRON	ENTAL HEA	T LOSS BO	JUNDA	RY	11	U.C.	ERI	170	限范											
******		CREEKER.		and the							8.20	0.8.5	4.6						a li ni	1.11.12
*********	**********			e te se	1.40	4.4	8.97.2		* *	N. 4.	10.00			1.4	199				0.0.0.	1.5.4
50583800	TEMP																			
20293901	0.0	311.00																		
	*******		e a a la c										a fa			1.0.0		a a car	1. 2. 11. 1	
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# REACTOR	VESSEL EN	IVI ORNMEN	TAL L	.05	51	植品	TAI	FER	0	IOE	FF	101	EN	Τ.						
*******	0		66666	140	4.5	63.0	5.01	5 5 5		5.8	2.2	5.54	40	5.25	351	5-15-1	6.15.4	3.8	424	0.5.6
ABABLEAS	1.197 10																			
x0544400	hel I Canan I																			
20294901	0.0	10.0																		
	*********		580.00		3.6		11 15	5.85.10	14.5		. 8. 8.	8 6 8	14.0	18.5	20	12	1.4.1	1.11	nin D.	16.5
a minima bi	**********	(Sugarenzy)	****				A 100							1.5						
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# CINCLE	DULET UPAP	PUBVEE																		
* 211101"E	MADE HEAL	LAWARD																		
操作的复数形式	*****	2.注导教教教教会会	资料资料	發展的	前原	2.8.4	**	新茶 4	1 發展	124	10.0	發展者	を発力	2.7	桥桥	作品	P 0 :	臣朝發	984	상관 환
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* HEAD CU	0005 NU. 1	*******			0.15	0.00		8 0 5	5 40 e	5 0 4	.0.0	6.6.1	141	0.9	0.9	4.6	ф e	0.00.6	100	0.0.0
* HEAD CU ********* 1351100	1 1 1 1 1 1	1	0 5 9 5	840	0.5	0 9 9	\$ 5	603	5 4 e		. 0 0	6.6.5	101	0.5	0.0	**	þ ö	t) № 6	194	0.0.0
* HEAD CU	1 0.000000	1		8 9 0 1 - 4	0.0.0	0 0 0 6 0 0		8 0 S	9 40 e		0.0	0.01	141	e v	0.0	e e	þ. 6	0 0 0	140	00
* HEAD CU 2000000000 1351100 1351101	1	1+00	0 5 0 U	2 4	03	600	*0	8 8 8 0	5 40 e	5 0 4		6.6.5	P 42 6	0.9	0.0	e e	p e	096	194	804
* HEAD CU ********** 1351100 1351101 1351102	1 0.0000006 1.9061006	1 1+00 5=01	0 5 9 U	8 8 0 1 + 4 1 + 3	03	600 600	* * *	8 8 8 0 0	9 49 C	5 0 6	. 0 0		P 42 6	0.0	0.9	**	0.0	0 0 6	100	004
* HEAD CU ********* 1351100 1351101 1351102 1351105	1 0.0000000 1.9061006 3.896300	1 1+00 5=01 5=01	0 9 A D	2 0 0 1 + 4 1 + 3 1 + 3	03	600 600 600	****	000			0.0			0.0	5.9	00	50	₽₽-6	1 Å Å	2 0 Q
* HEAD CU ********* 1351100 1351101 1351102 1351105 1351104	1 0.00000000 1.9061000 3.8963000	1 1+00 1=01 1=01	0 5 A 5	0 0 4 3 3 3 4 3 3 4 3 4 3 4 3 4 3 4 3 4	03	6000 6000 6000	*****	00000	3 4 d		. 0 0			0.0	9.9	00	р. 6-	0 - 6	194	6 Ø Ø
* HEAD CU ********* 1351100 1351102 1351105 1351104	1 0.00000000 1.9061000 3.8963000 5.9396000	1 1+00 1=01 1=01 1=01	0 5 A 5		03	600 600 600 800	****	00000			. 0 0	6.64	1 & I	0.5	9.9	**	þ.e.	8 1 1 1	1 û R	00
* HEAD CU ************************************	1 0.0000000 1.9061008 3.8963008 5.9396008 7.9020008	1 +00 =01 =01 =01 =01 =01	0 5 A D		103 163 163 132 133	6000 6000 6000 6000	*****	00000			. 0 0	8.8.9		0.4	2.9		ф. 6	8 8 6	100	808
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<pre>* HEAD CU ************************************</pre>	1 0.00000000 1.9061000 3.8963000 5.9396000 7.9020000 1.0000000	1 +00 =01 =01 =01 =01 =01 =01 =01 =01			033163823300	600 600 600 600 600 600	* * * * * * *	000000						0.0	5.0	00	00	₽ ₽ 6	100	0.80
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1351504 4 1156302-64	3.400000CL*01
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19515X/ H HALLMAN AT	4+2040006-01
12010// 7:934670E=01	6.9920005+01
1991207 1:000000E+00	1.000000E+00
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* HEAD CURVE NO.6	
带拉斯拉拉拉拉斯拉拉拉拉拉拉拉拉拉拉拉拉拉拉拉拉拉拉拉拉拉拉拉拉拉拉拉拉拉拉	144040404040404040404040404040400000000
1351600 1	6
1351601 0.0000002E+00	9.3427005-01
1351602 9.109900F=02	1.229000F-01
1351603 1.865090F+01	8.0430AAE+A+
1351604 2.717620F=01	0 76000-01 AL
1351605 4.5527205-01	0.1000000-01
1351606 5.7460605-01	8.432000E=01
1351607 7 100000-01	8.322VQQE=01
13517001 1.403100E=01	8.466000E=01
1001005 7:6661906=01	8.469003E=01
1001009 8.714710E=01	8.838000E=01
1331010 1:000000E+00	1.000000E+00
Bobook	0.8.8.9.9.9.9.9.9.9.9.9.9.9.9.9.9.9.9.9.
* HEAD CURVE NO.7	
**************	0
1351700 1	7
1351701 ~1.000000E+00	+1.000000F+00
1351702 -8.00000005-01	#6.300000E+01
1351703 -6.000000F-01	=3.000000E=01
1351704 -4.00000000-01	-2.0000000000
1351705 -2 0300305-01	
1351706 0.000000000000	1.2000005=01
	5.200000F=01
* UEVE %1005 10 4	>>>>>>>>>>>>>>>>>>>>>>>>>>>>>>>>>>>>>>
* MEAD SURVE MI.8	
**********	HAMANAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAA
1351800 1	8
1351801 -1.000000E+00	-1.CODOCOE+00
1351802 +8.000000E=01	-9.700000E-01
1351803 ~6.00000F=01	=9.500000E-01
1351804 -4.000000E-01	-8.800000F-01
1351805 -2.000000E-01	=8-000000E=01
1351806 0.0000005+00	-6.7000005-01

& SINGLE PHASE TOPOLIE DATA	····································
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S TROALE MUDUE NA 4	***************************************
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1351000	的现在在在你的你的你的你的你的你你你你你你你你你你你你你你你你你你你你你。 你们你你你你你你你你你你
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1352501 -1 0000000000	
1353503 -3 00000000000	-1.000000000000
1959503 -1 000000E=01	-A.000000E-01
13535203 -1.000000E=01	-2.00000E=01
T995904 0*00000F+00	-4.500000E=01
***************************************	5 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
* TURQUE CURVE NO.8	
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1935601 =1*0000000.+00	-1.0C0000E+00
1992602 -2.5000001.*01	-9.070000E-01
1002003 -8.000000E=02	-\$.000000E=01
1352604 0.000000E+00	-6.70000E+01
00000000000000000000000000000000000000	0.000000000000000000000000000000000000
* THOMPHA SE MULTIPLIER DATA L	3+6 TEST DATA
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* HEAD CURVE	
******************	\$*************************************
1353000 0	
1353001 0.00000E+00	0.000000000000
1353002 1.000000E-01	0.000000E+00
1353003 2.000000E=01	1.000000E+01
1353004 3.00000E-01	2.0000005+01
1353005 3.500000E-01	3.0000006-01
1353006 4.000000E-01	6.0000005-01
1353007 5.000000E-01	6.0000005-01
1353008 6.0000006-01	6.0000000000
1353009 7.000000F-01	6.0000005-01
1353010 8.000000F=01	5.0000005=01
1353011 9-000000E-01	3.0000005-01
1353012 1.000000000000	0.0000000000000000000000000000000000000
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TOROUF CURVE	***************************************
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<pre>> TDRQUE CURVE ************************************</pre>	0.000000E+00
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<pre>> TURQUE CURVE ************************************</pre>	0.000000E+00 0.000000E+00 1.000000E=01 3.00000E=01
<pre>> TURQUE CURVE ************************************</pre>	0.000000E+00 0.000000E+00 1.000000E+01 3.000000E+01 5.000000E+01
<pre>> TURQUE CURVE ************************************</pre>	0.000000E+00 0.000000E+00 1.000000E+01 3.000000E+01 5.000000E+01 7.500000E=01
<pre>b TURQUE CURVE ************************************</pre>	0.000000E+00 0.000000E+00 1.000000E+01 3.000000E+01 7.500000E+01 7.500000E+01
<pre>b TURQUE CURVE ************************************</pre>	0.000000E+00 0.000000E+00 1.000000E+01 3.000000E+01 7.500000E+01 7.500000E+01 7.500000E+01 7.500000E+01
<pre>> TURQUE CURVE ************************************</pre>	0.000000E+00 0.000000E+00 1.000000E+01 3.000000E+01 7.500000E+01 7.500000E+01 7.500000E+01 7.500000E+01 7.500000E+01 7.500000E+01
> TORQUE CURVE ************************************	0.000000E+00 0.000000E+00 1.000000E+01 3.00000E=01 5.00000E=01 7.500000E=01 7.500000E=01 7.500000E=01 7.500000E=01 7.500000E=01 7.500000E=01
> TORQUE CURVE ************************************	0.000000E+00 1.000000E+00 1.000000E+01 3.00000E=01 5.00000E=01 7.500000E=01 7.500000E=01 7.500000E=01 7.500000E=01 5.00000E=01 5.00000E=01 5.00000E=01 5.00000E=01 5.00000E=01 5.00000E=01
> TORQUE CURVE >>>>>>>>>>>>>>>>>>>>>>>>>>>>>>	0.000000E+00 0.000000E+00 1.000000E+00 1.000000E+01 3.000000E+01 7.500000E+01 7.500000E+01 7.500000E+01 7.500000E+01 7.500000E+01 0.00000E+01 0.00000E+00
TORQUE CURVE ************************************	0.000000E+00 0.000000E+00 1.000000E+00 1.000000E+01 3.000000E+01 7.500000E+01 7.500000E+01 7.500000E+01 7.500000E+01 7.500000E+01 0.00000E+00 0.00000E+00
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1354202	1 00000000000	
	T*0000005+05	1.000000+00
*********	*****************	***************************************
# HEAD	CURVE NO. 3	
*****	00000000000000000000000000000000000000	***************************************
1354300	1	3
1354301	000000E+00	-1.160(00+00
1354302	-9.000000E-01	+1.240000+00
1354303	-8.0000002-01	-1.770000+00
1354304	-7.000000E-01	+2,360000+00
1354305	-6.000000E-01	-2.790000+00
1354306	-5.0000005-01	-2,910000+00
1354307	-4 000000E=01	-2.67000000
1354300	-2 60000000-01	-2.070000+00
1982900	-2.50000000-01	
15813107	-1.000000L-01	=>.00000=01
7334570	0.000005.000	0.00000+00
800086565		***********************
* HEAD	CURVE NO, 4	
******		***************************************
1354400	1 4 H H H H H H H H H H H	4
1354401	-1.00000000000	-1.160000+00
1354402	-9.00000E-01	-7.800000-01
1354403	-8.00000E-01	-5.000000-01
1354404	-7.00000E-01	-3.100000-01
1354405	-6.000000E-01	=1.700000=01
1354406	-5.000000E-01	-8.000000-02
1354407	-3.500000F-01	0.000000+00
1354408	-2.000000E-01	5.00000-02
1354400	-1.0000005-01	8.000000-02
1354410	0.00000000000	1.100000-02
SSARBARE.		1.10000-01
	CURVE NO E	, , , , , , , , , , , , , , , , , , ,
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********		00000000000000000000000000000000000000
1224200	1	
3 5 5 4 5 5 5 5		
1354501	0.000000000000	0.00000E+00
1354501 1354502	0.000000E+00 2.000000E+01	0.00000E+00 -3.400000E-01
1354501 1354502 1354503	0.000000E+00 2.000000E-01 4.000000E-01	0.000000E+00 -3.400000E-01 -6.500000E-01
1354501 1354502 1354503 1354504	0.000000E+00 2.000000E+01 4.000000E=01 6.000000E=01	0.000000E+00 -3.400000E-01 -6.500000E-01 -9.300000E-01
1354501 1354502 1354503 1354504 1354505	0.000000E+00 2.000000E-01 4.000000E-01 6.000000E-01 B.000000E-01	0.000000E+00 -3.400000E-01 -6.500000E-01 -9.300000E-01 -1.190000E+00
1354501 1354502 1354503 1354504 1354505 1354506	0.000000E+00 2.000000E-01 4.000000E-01 6.000000E-01 8.000000E-01 1.000000E+00	0.000000E+00 -3.400000E-01 -6.500000E-01 -9.300000E-01 -1.190000E+00 +1.470000E+00
1354501 1354502 1354503 1354504 1354505 1354506	0.000000E+00 2.000000E=01 4.000000E=01 6.000000E=01 8.000000E=01 1.000000E+00	0.000000E+00 -3.400000E-01 -6.500000E-01 -9.300000E-01 -1.190000E+00 +1.470000E+00
1354501 1354502 1354503 1354504 1354505 1354506 **********	0.000000E+00 2.000000E=01 4.000000E=01 6.000000E=01 8.000000E=01 1.000000E=00 1.000000E+00	0.000000E+00 -3.400000E-01 -6.500000E-01 -9.300000E-01 -1.190000E+00 -1.470000E+00
1354501 1354502 1354503 1354504 1354505 1354506 ********** * HEAD	0.000000E+00 2.000000E=01 4.000000E=01 6.000000E=01 B.000000E=01 1.000000E=00 1.000000E+00 CURVE NO. 6	0.000000E+00 -3.400000E-01 -6.500000E-01 -9.300000E+01 -1.190000E+00 -1.470000E+00
1354501 1354502 1354503 1354504 1354505 1354506 ********* * HEAD *********	0.000000E+00 2.000000E=01 4.000000E=01 6.000000E=01 8.000000E=01 1.000000E+00 *****************************	0.000000E+00 -3.400000E-01 -6.500000E-01 -9.300000E-01 -1.190000E+00 -1.470000E+00 -1.470000E+00
1354501 1354502 1354503 1354505 1354505 1354506 ********* * HEAD ********* 1354600 1354601	0.000000E+00 2.000000E=01 4.000000E=01 6.000000E=01 8.000000E=01 1.000000E+00 *****************************	0.000000E+00 -3.400000E-01 -6.500000E-01 -9.300000E+00 -1.470000E+00 -1.470000E+00 -1.470000E+00 -1.470000E+00 -1.470000E+00
1354501 1354502 1354503 1354505 1354505 1354506 ********* * HEAD ********* 1354600 1354601 1354602	0.000000E+00 2.000000E=01 4.000000E=01 6.000000E=01 1.000000E=01 1.000000E+00 CURVE NO. 6 0.000000E+00 1.000000E+00 1.000000E+00	0.000000E+00 -3.400000E-01 -6.500000E-01 -9.300000E+00 -1.470000E+00 -1.470000E+00 -1.100000E-01 1.300000E-01
1354501 1354502 1354503 1354505 1354505 1354506 ********** * HEAD ********* 1354600 1354601 1354602	0.000000E+00 2.000000E=01 4.000000E=01 6.000000E=01 1.000000E=01 1.000000E+00 0.000000E+00 1.000000E+00 1.000000E+00 1.000000E=01	0.000000E+00 -3.400000E-01 -6.500000E-01 -9.300000E+00 -1.470000E+00 -1.470000E+00 -1.00000E-01 1.300000E-01 1.500000E-01
1354501 1354502 1354503 1354505 1354505 1354506 ********** * HEAD ********* 1354600 1354601 1354602 1354603	0.000000E+00 2.000000E=01 4.000000E=01 6.000000E=01 1.000000E=01 1.000000E+00 0.000000E+00 1.000000E+00 1.000000E=01 2.500000E=01	0.000000E+00 -3.400000E-01 -6.500000E-01 -9.300000E+00 -1.470000E+00 -1.470000E+00 -1.00000E-01 1.300000E-01 1.500000E-01 1.500000E-01
1354501 1354502 1354503 1354504 1354505 1354506 ******** HEAD ******** 1354600 1354602 1354602 1354604 1354604	0.000000E+00 2.000000E=01 4.000000E=01 8.000000E=01 1.000000E=01 1.000000E+00 0.000000E+00 1.000000E+00 1.000000E=01 2.500000E=01 4.000000E=01	0.000000E+00 -3.400000E-01 -6.500000E-01 -9.300000E+00 -1.470000E+00 -1.470000E+00 -1.470000E-01 1.300000E-01 1.300000E-01 1.300000E-01 1.300000E-01 1.300000E-01
1354501 1354502 1354503 1354504 1354505 1354506 ******** 1354600 1354600 1354602 1354602 1354604 1354605	0.000000E+00 2.000000E+00 4.000000E=01 6.000000E=01 1.000000E+00 0.000000E+00 1.000000E+00 1.000000E+00 1.000000E=01 2.500000E=01 4.000000E=01 5.000000E=01	0.000000E+00 -3.400000E-01 -6.500000E-01 -9.300000E+00 -1.470000E+00 -1.470000E+00 -1.470000E-01 1.300000E-01 1.300000E-01 1.300000E-01 1.300000E-02 -0.0000E-02
1354501 1354502 1354503 1354504 1354505 1354506 ********* 1354500 1354600 1354602 1354602 1354602 1354605 1354605 1354605	0.000000E+00 2.000000E+00 4.000000E+01 6.000000E+01 1.000000E+00 0.000000E+00 1.000000E+00 1.000000E+00 1.000000E+01 2.500000E+01 4.000000E+01 5.000000E+01	0.000000E+00 -3.400000E-01 -6.500000E-01 -9.300000E+00 -1.470000E+00 -1.470000E+00 -1.470000E-01 1.300000E-01 1.300000E-01 1.300000E-01 1.300000E-01 1.300000E-02 -4.00000E-02
1354501 1354503 1354504 1354505 1354506 ************************************	0.000000E+00 2.000000E+00 4.000000E+01 6.000000E+01 1.000000E+00 *****************************	0.000000E+00 -3.400000E-01 -6.500000E-01 -1.19000E+00 -1.470000E+00 -1.470000E+00 -1.30000E-01 1.30000E-01 1.500000E-01 1.500000E-01 300000E-01
1354501 1354502 1354503 1354505 1354506 ************************************	0.000000E+00 2.000000E+00 4.000000E+01 6.000000E+01 1.000000E+00 1.000000E+00 1.000000E+00 1.000000E+00 1.000000E+01 2.500000E+01 4.000000E+01 5.000000E+01 6.000000E+01 8.000000E+01 8.000000E+01	0.000000E+00 -3.400000E-01 -6.500000E-01 -9.30000E-01 -1.19000E+00 =1.470000E+00 =0.0000E-01 1.30000E-01 1.500000E-01 1.500000E-01 1.30000E-01 -5.10000E-01 -5.10000E-01
1354501 1354503 1354504 1354505 1354506 *** HEAD ******** 1354600 1354600 1354602 1354602 1354605 1354605 1354605 1354607 1354607 1354608	0.000000E+00 2.000000E+00 4.000000E=01 6.000000E=01 1.000000E+00 *****************************	0.000000E+00 -3.400000E-01 -6.500000E-01 -9.30000E-01 -1.470000E+00 =0.470000E+00 =0.470000E-01 1.300000E-01 1.300000E-01 1.500000E-01 1.500000E-01 -5.100000E-01 -9.100000E-01 -9.100000E-01
1354501 1354503 1354503 1354505 1354506 ************************************	0.000000E+00 2.000000E+00 4.000000E+01 6.000000E+01 1.000000E+00 *****************************	0.000000E+00 -3.400000E-01 -6.500000E-01 -9.30000E-01 -1.470000E+00 ===================================
1354501 1354503 1354503 1354505 1354505 1354506 ************************************	0.000000E+00 2.000000E=01 4.000000E=01 8.000000E=01 1.000000E+00 0.000000E+00 1.000000E+00 1.000000E=01 2.500000E=01 4.000000E=01 5.000000E=01 6.000000E=01 8.000000E=01 8.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01	0.000000E+00 -3.400000E-01 -6.500000E-01 -9.30000E-00 -1.470000E+00 -1.470000E+00 -1.470000E-01 1.300000E-01 1.300000E-01 1.500000E-01 -5.100000E-01 -5.100000E-01 -1.47000E+00 ***********************************
1354501 1354503 1354503 1354505 1354506 ************************************	0.000000E+00 2.000000E=01 4.000000E=01 8.000000E=01 1.000000E+00 1.000000E+00 1.000000E+00 1.000000E=01 2.500000E=01 4.000000E=01 5.000000E=01 6.000000E=01 8.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 2.500000E=01 0.000000E=01 0.000000E=01 0.000000E=01 0.000000E=01 0.000000E=01 0.000000E=01 0.000000E=01 0.000000E=01 0.000000E=01 0.000000E=01 0.000000E=01 0.000000E=01 0.000000E=01 0.000000000E=01 0.000000E=01 0.000000E=01 0.000000E=01 0.000000E=01 0.000000E=01 0.000000E=01 0.000000E=01 0.000000000000000E=01 0.0000000000000000000000000000000000	0.000000E+00 -3.40000E=01 -6.500000E=01 -1.19000E=00 +1.470000E+00 ***********************************
1354501 1354503 1354503 1354505 1354506 ************************************	0.000000E+00 2.000000E=01 4.000000E=01 8.000000E=01 1.000000E+00 1.000000E+00 1.000000E+00 1.000000E=01 2.500000E=01 4.000000E=01 5.000000E=01 6.000000E=01 8.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 2.500000E=01 7.000000E=01 7.000000E=01 1.000000E=01 7.000000E=01 7.000000E=01 7.000000E=01 7.000000E=01 7.000000E=01 7.000000E=01 7.000000E=01 7.000000E=01 7.000000E=01 7.00000000E=01 7.0000000E=01 7.000000E=01 7.000000E=01 7.000000E=01 7.000000E=01 7.000000E=01 7.000000E=01 7.000000E=01 7.000000E=01 7.000000E=01 7.000000E=01 7.000000E=01 7.000000E=01 7.000000000000000000E=01 7.00000000000000000000000000000000000	0.000000E+00 -3.40000E+01 -6.50000E+01 -1.19000E+00 +1.47000E+00 ***********************************
1354501 1354502 1354503 1354505 1354506 ************************************	0.000000E+00 2.000000E=01 4.000000E=01 8.000000E=01 1.000000E+00 1.000000E+00 1.000000E+00 1.000000E=01 2.500000E=01 4.000000E=01 5.000000E=01 6.000000E=01 8.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.00000000E=01 1.0000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 0.000000E=01 0.000000E=01 0.000000E=01 0.000000000000000000E=01 0.0000000000000000000000000000000000	0.000000E+00 -3.400000E-01 -6.500000E-01 -1.190000E+00 +1.470000E+00 +1.470000E+00 +**********************************
1354501 1354503 1354503 1354505 1354505 1354506 ************************************	0.000000E+00 2.000000E=01 4.000000E=01 8.000000E=01 1.000000E+00 1.000000E+00 1.000000E+00 1.000000E=01 2.500000E=01 4.000000E=01 5.000000E=01 6.000000E=01 8.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01 1.000000E=01	0.000000E+00 -3.400000E-01 -6.500000E-01 -1.190000E+00 +1.470000E+00 ***********************************
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TORQUE CURVE NO. 2	

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7999000 5	가지, 물러 그녀 안 있지, 않아, 아이들 것이 같아요. 그는 것이 가지 않는 것이 같아. 가지 않는 것이 없는 것이 없는 것이 없는 것이 없다. 가지 않는 것이 없는 것이 없는 것이 없는 것이 없다. 것이 없는 것이 없다. 것이 없는 것이 없다. 것이 없는 것이 없 않는 것이 없는 것이 않이 없는 것이 없 않이
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1355002 1.000000E+00	1.0000007400
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* TUKQUE ÇURVE NO. 3	
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1355100 2	
1355101 -1.0000005+00	5 0019000.00
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1355103 =6.063800E-01	1.097500E+00
1355104 -0.40686	0.82200
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* TOROUE CURVE NO. A	
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1355200 2	
1355201 -1.000000E+00	1.984300E+00
1355202 -8.223400E-01	1 8308005+00
1355305	
T000500 -0*021700F-0T	1.682400E*00
1355204 -4,585300E=01	1.557000E+00
1355205 -2.670230E-01	1-4362005+00
1355206 -1.7610705-01	3 3870005+00
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1353207 =8.931000E=02	1.348100E+00
1355208 0.000000E+00	1.233610E+00
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1355300 2	5
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1355303 5.000000E-01	0.0000000000000000000000000000000000000
1355304 1.000000E+00	3.569000E=01

& TOPOUE CUDVE NO. 4	
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1355400 2	6
1355401 0.0000005+00	1,2336105+00
1968A00 0 011800F 00	4.6222020200
100002 9.0643006-02	1*1402006+00
1355403 1.885690E-01	1.109600E+00
1355404 2.734700E-01	1.041600E+00
1355405 4.5846905-01	8-958000F+01
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1355407 7.381600E=01	
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1355408 7.685200E-01	6.134000E=01 5.849000E=01
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20500100	SGLVL	SUM		1	.0				0	.0				2							
20500101	0.0	0.8288		V	010	SF.			5	00	010	00	00								
20500102		0.8288		V	010	F			5	05	011	001	00								
20500103		0.8288		V	010	F			5	07	010	00	00								
20500104		0.6096		V	010	F			5	08	01	00	00								
20500105		0.6096		V	010	SF			5	10	01	00	00								
20500106		0.6096		V	010	3F			5	10	52	00	00								
20500107		0.6036		V	1011	3F			6	10	03	00	00								
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# 003	REACTOR VES	SEL LEVE																	÷.,		
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20500300	RXCLVL	SUM			1.0	£ -				0.1	Q			1							
20500301	0.0	1.566			VOI	DF			1	25	501	1.00	500	5							
20500302		0.843			VOI	DF				25	001	100	000	3							
20500303		0.559			VOI	DF				24	503	100	003	5							
20500304		0.559			VOI	DF				24	00	100	000	5							
20500305		0.375			VOI	DE				23	20	1.0	000	8							
20500306		0.2705			voi	DE				23	10	10	0.00	6							
20500500		0.2705			vai	NE				23	00	10	0.01	6							
20500301		0 0705			VOI	UF				52	00	10	AA!	5							
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20200310		0+2195			VU.	IDF				66	10	10	20	× .							
20500311		0.520			YU.	IOP				22	20	10	00	2							
20500312		0.360			VD.	IDF				21	20	10	00	2							
20500313		0.370			VO	IDF				22	00	10	00	2						÷	
800000000	*****	*******	000	***	0.00	体操作	000	* #	0.0	0.0	2.0	* *	8.5	9.0	0.0	8.81	000	1 Q 1	4.5	489	10.5
# 004	REACTOR VES	SSEL DOWN	COM	ER	11	LEI	VEL													-	
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20500400	DCMR1LVL	SUM			1.	0				0.	0				1						
20500401	0.0	0.330			VO	101	÷ .			20	00	10	000	0							

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20500402 20500404 20500404 20500405 20500405 20500405 20500405 20500405 20500405 20500405 20500405	LCOP SEAL	0.424 0.958 0.958 0.958 0.958 0.958 0.350 0.370 0.370 0.370 0.570 0.570	VOIDF VOIDF VOIDF VOIDF VOIDF VOIDF VOIDF VOIDF	202010003 204010000 206010000 208010003 210010000 215010000 220010000	
20500500	LPSLUP	SUM	1.0	0.0	1
20500501	0.0	0.284175	VOIDF	120010000	
20500502		0.356	VOIDE	118030000	
20500503		0.689	VOIDF	118020000	
20500504		0.498	VOIDF	118010000	
******	*********			**********	
* 006	LOOP SEAL	DOWNSTREAM	LEVEL		
********	******	******	000000000000	000000000000000	
20500600	LPSLOWN	SUM	1.0	0.0	1
20500601	0.0	0.284175	VOIDE	120010000	
20500602		0.2605	VOIDE	125010000	
20500603		0.2285	VOIDF	130010000	
20500604		0.2605	VOIDF	155010000	
20500605		0.2285	VOIDF	160010000	
· 문학 전 전 전 전 전 전 전 전 전 전 전 전 전 전 전 전 전 전	*******	********	****	*****	00000000000000000000000000000000000000
₽ 007	REACTOR VES	SEL DOWNCOME	R 2 LEVEL		
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20500700	DCMR2LVL	SUM	1.0	0.0	1
20500701	0.0	0.330	VOIDE	280010000	
20500702		C * 424	VOICF	282010000	
20500703		0.958	VOIDF	284010000	
20500704		0+958	VDIDE	286010000	
20500705		0.958	VUIDE	285010000	
20000700		0.938	VUIDE	Sa0010000	
20000101		0.350	VUICE	215010000	
20300100		0.010	VUIDE	550010000	
8 041-07	E DDIVADV CV	CTEN NACE PA	1 MIN 4 MMM	16095999999988	66956060608069 <u>6</u> 56566
	BERBERERERERERE	BABBBBBBBBBBBBBB	SBOB SEALARS		
* 061	INTACT LOC	IP HAT LES M	116C	**********	****************
	5666666666666666	000000000000000000000000000000000000000	00000		**************
20506100	11 HLMASS	SUM	1.0	1.0 1	
20506101	0.0	9.74648-2	RHO	00010000	
20506102		0.1035956	RHO	05010000	
20506103		3.03000-2	RHO	110010000	
20506104		9.00000-2	RHC	112010000	
20506105		5.70000-2	RHO	112020000	
****					**************
# 062	STEAM GENE	EATOR PRIMARY	MASS		
******	***********	************	*********	****	************
20506200	SGPRIASS	SUM	1.0	0.0 1	
20506201	0.0	0.335000	RHO	114010000	
20506202		0.136202	RHO :	115010000	
20506203		9-20496-2	RHO	115020000	
20506204		9.20496-2	RHO	115030000	
20506205		6.96412+2	RHO	115040000	
20506206		6.96412-2	RHO	115050000	
20506207		9.20496-2	RHO	115060000	
20506208		9.20496-2	RHU	115070000	
20506209		0.136202	RHO	115080000	
20506210)	0.335000	RHO	116010000	
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P 063	PUMP SUCTI	ON PIPING	MASS		
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20506300	PMPSUASS	SUM	1.0	0.0	
20506301	0.0	4.37000-2	RHD	118010300	
20506302		4.62000-2	RHD	118020000	
20506303		3.34405-2	RHU	118030000	
20506304		4.81840-2	RHO	120010000	
20506305		6.13000-2	RHO	152010000	
20506306		1.89000-2	RHO	130010000	
20506307		6.13000-2	RHD	155010000	
20506308		7*84000=5	PHU	160010000	
*********	***********	1	898999989	************	# 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
* 064	INTACI LUC	IN COLD LES	CEAM	a la construction de la construction de la construcción de la construc	
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20000400	ILCLMAD5	S DECAR A	1.0		÷
20000001	0.40	7 . 70000=Z	6.6.5	133010000	
20300402		1:02/32=2	1 F1 ()	140010000	
20000400		6.22000-2	550	145010000	
20505404		3.14844=2	KHU	152010000	
20000000		A*A0000=5	PC 255 5 3	162010000	
20306406		1.00120+2	NHO DUD	110010000	
20506401		3.34405=2	RHU	175010000	
20506408		3.88642*2	KHU	176010000	
20506409		1.30368=2	RHO	150010000	
20505410		0+40340=Z	RHU	182010000	
*********		21 CUTO DI CUI			82555555555555555555555555 825555555555
* 002	DUNNELINER	LUNER PLECK			
20404400	Dri Dulce	CIN	1 0	0.0	1
20506500	0.0	4.28000-2	e-0	200010000	•
20506503		4.28000-2	ENU	280010000	
20506503		5.50000-2	040	202010000	
20506504		5.50000-2	RHO	282010000	
20506505		6-80180-2	RHO	204010000	
20506506		6.80180-2	PHO	284010000	
20506507		6.80180-2	RHO	206010000	
20506508		6-80180-2	RHO	286010000	
20506509		6.80180-2	RHO	208010000	
20506510		6-80180-2	890	288010000	
20506511		6.80180-2	RHD	210010000	
20506512		6.80180-2	RHD	290010000	
20506513		2.66400-1	RHO	215010000	
20506514		2.92300-1	RHO	220010000	
*******	**********	***********		00000000000000	94544664000, 4446444
♥ 067	AVERAGE/C	ORE UPPER P	LENUM MAS	S	
******	******	*******	********	*****	04444444444444444444
20506700	ACUPMASS	SUM	1.0	0.0	1
20506701	0.0	1.30000-1	RHO	225010000	
20506702		3.86929-2	RHO	227010000	
20506703		3.86929-2	RHD	228010000	
20506704		3.86929-2	RHO	229010000	
20506705		3.86929-2	RHO	230010000	
20506706		3.86929-2	RHO	231010000	
20506707		5.22596-2	RHO	232010000	
20506708		8.38500-3	RHO	226010000	
20506709		8.38500-3	RHO	226020000	
20506710		9.85500-3	RHD	226030000	
20506711		1.66023-1	RHO	240010000	
20506712		1.66023-1	RHO	245010000	
20506713		9.61020-2	RHO	250010000	
20506714		1.28100-1	RHO	251010000	
20506715		4.19680-1	EH0	255010000	

*****		(你爸爸爸爸爸爸爸爸爸爸??)	*********	******	
# 068	BROKEN	LOOP HOT LEG	MASS(TO BRE	AK PLANES	
*******		000000000000000000			000000000000000000000
20506800	BLHLMAS	IS SUM	1.0	0.0	1
20506801	0.0	5.55384-2	RHD	300010000	*
20506802		4.42532-2	RHO	305010000	
20506803		6.68000-2	RHO	310010000	
20506804		7.78800-3	RHO	315010000	
20506805		1.72500-1	RHO	315020000	
20506806		8.98000-2	RHD	315030000	
20506807		8.98000-2	840	315040000	
20506808		1.72500-1	RHO	315050000	
20506809		2.02000+2	RHO	315040000	
20506810		4.56000-2	RHO	315070000	
20506811		1.98000-2	RHO	315080000	
20506812		1.16500-1	RHO	380010000	
20506913		2.30000-2	RHO	380020000	
20506814		4.89000-2	RHO	380030000	
*****	*****	**********			****************
* 069	BROKEN	LOOP COLD LES	MASS(TO BR	REAK PLANES)
*******	***	***********	**********		
20506900	BLCLMAS	SS SUM	1.0	0.0	1
20506901	0.0	4.75183-2	RHO	335010000	
20506902		4.42532-2	RHO	340010000	
20506903		4.43800-2	RHO	345010000.	
20506904		2.33600-2	RHD	350010000	
20506905		2.79000-2	RHO	370010000	
20506906		7.0000-2	RHO	370020000	
20506907		1.16500-1	RHO	370030000	
****	****	*****	\$\$\$\$\$\$\$\$\$		***************
* 070	PRESSU	RIZ ER	MASS		
*****	*****	********	********		***********
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20507000 20507001 20507002	PZERMA	SS SUM 3.33500-3 3.33500-3	1.0 RHD RHD	0.0 400010000 405010000	59559855555555555555555555555555555555
20507000 20507001 20507002 20507003	PZERMA	SS SUM 3.33500-3 3.33500-3 3.33500-3	************ 1.0 RHO RHO RHO	0.0 400010000 405010000 405020000	59559955555555555555555555555555555555
20507000 20507001 20507002 20507003 20507003	PZERMA 0.0	SS SUM 3.33500-3 3.33500-3 3.33500-3 6.84000-2	***** 1.0 RHO RHO RHO RHO RHO	0.0 400010000 405010000 405020000 415010000	59559555555555555555555555555555555555
20507000 20507001 20507002 20507003 20507003 20507004 20507005	******* PZERMA 0.0	SS SUM 3.33500-3 3.33500-3 3.33500-3 6.84000-2 8.38000-2	***** 1.0 RHO RHO RHO RHO RHO RHO	0.0 400010000 405010000 405020000 415010000 415020000	59559555555555555555555555555555555555
20507000 20507001 20507002 20507003 20507004 20507005 20507005	******* PZERMA 0.0	SS SUM 3.33500-3 3.33500-3 3.33500-3 6.84000-2 8.38000-2 2.24255-1	************ 1.0 RHD RHD RHD RHD RHD RHD RHD RHD	0.0 400010000 405010000 405020000 415010000 415020000 415030000	59559555555555555555555555555555555555
20507000 20507001 20507002 20507003 20507004 20507005 20507005 20507006 20507007	****** PZERMA 0.0	SS SUM 3.33500-3 3.33500-3 3.33500-3 6.84000-2 8.38000-2 2.24255-1 2.98987-1	A A A A A A A A A A A A A A A A A A A	0.0 400010000 405010000 405020000 415010000 415020000 415030000 415040000	59559555555555555555555555555555555555
20507000 20507001 20507002 20507003 20507004 20507005 20507006 20507006 20507006	****** PZERMA 0.0	SS SUM 3.33500-3 3.33500-3 3.33500-3 6.84000-2 8.38000-2 2.24255-1 2.98987-1 2.24255-1	**************************************	0.0 400010000 405010000 405020000 415010000 415020000 415030000 415040000 415050000	5.55.55.55.55.55.55 1 1
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+ + + + + + + + + + + + + + + + + + +	PZERMA 0.0	SS SUM 3.33500-3 3.33500-3 3.33500-3 3.33500-3 6.84000-2 8.38000-2 2.24255-1 2.98987-1 2.24255-1 7.32000-2 1.42000-2	**************************************	0.0 400010000 405010000 405020000 415010000 415020000 415030000 415040000 415050000 415060000 415060000 415060000 415070000	5.55.55.55.55.55.55 1
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+ * * * * * * * * * 20507000 20507001 20507002 20507003 20507005 20507005 20507006 20507006 20507009 20507010 20507010 20507011 * * * * * * * * * * 20507700 20507700 20507701 20507702 20507703	******* PZERMA 0.0 ******* TOTAL ******* TCUPMA 0.0	SS SUM 3.33500-3 3.33500-3 3.33500-3 3.33500-3 6.84000-2 8.38000-2 2.24255-1 2.98987-1 2.24255-1 7.32000-2 1.42000-2 1.42000-2 1.42000-2 1.42000-2 SS SUM 6.99977-3 6.99977-3 6.99977-3	**************************************		**************************************
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*********************************	******** PZERMA 0.0 ******** TOTAL ******** TCUPMA 0.0	SS SUM 3.33500-3 3.33500-3 3.33500-3 3.33500-3 6.84000-2 8.38000-2 2.24255-1 7.32000-2 1.42000-2 1.5000-2 1.5000-2 1.00000-2 1.0000000-2 1.000000000000000000000000000000000000	1.0 RHD RHD RHD RHD RHD RHD RHD RHD	0.0 400010000 405010000 405020000 415010000 415020000 415040000 415050000 415060000 415060000 415060000 415070000 415070000 233010000 233010000 235010000 236010000 236010000 236010000 236010000 236010000 067	**************************************
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A607053				1.0	CN	INLVAN	11					
0701700				1.0	CV.	TRLVAR	0.4					
020140*				1.0	CN.	TRLVAR	6.8					
C507902				1.0	Ch	TRLVAP	69					
0507905				1.10	01	TRI VAR	70					
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20507402				2.0101		PHO.	5	150300	00			
20507403				5.0767	5-7	RHU DUID		150400	000			
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* 073 STEAM GENE 20507300 CGDCMASS 20507301 0.0 20507302 20507303 20507304 20507305 20507306	PATOR DOWNED SUM 1.02770 1.00850 2.21070+1 1.41427-1 1.41427-1	HER MASS 1.0 RHO RHO RHO RHO RHO RHO RHO RHO RHO RHO	0.0 505010000 505010000 508010000 510010000 510010000 510020000	1
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A N76 CTEAU CENE	DATIO BALLES	NACC NACC	**********	******************
	5655555555555	10000		**************
20507400 CGBLMASS 20507401 0.0 20507402 20507403 20507404 20507405 20507405 20507406 20507407	SUM 5.07675-1 5.07675-1 5.07675-1 5.07675-1 2.59406-1 2.41897-1 2.00114-1	1.0 RHD RHD RHD RHD RHD RHD RHD RHD RHD RHD	0.0 515010000 515020000 515030000 515040000 515050000 515060000 520010000	1
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BIBLIOGRAPHIC DATA SHEET	NUREG/1A=0045
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O. SUPPLEMENTARY NOTES	
This report documents the results and conclusions of the RELAPS/ the analysis of LOCE Test L2-5. The objective of this assessment systematic assessment of RELAP5/MOD2 Code relative to code devel	OD2 code assessment in to tudy is to provide
and the enhancement of user guidelines.	opment, code improvement
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and the enhancement of user guidelines. 12. KEY WORDS DESCRIPTORS (Lui more or present that will summ researches in tecaning the report) ICAP Program, RELAP5/MOD2, L2-5	13 AVAILABILITY STATE MEN 13 AVAILABILITY STATE MEN 11 limited 1. SECURITY CLASSIFICATION Unclassified 17 hu Proon/ Unclassified

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