

NUREG/IA-0059



# International Agreement Report

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## Assessment of RELAP5/MOD2 Against Natural Circulation Experiments Performed with the REWET-III Facility

Prepared by  
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Office of Nuclear Regulatory Research  
U.S. Nuclear Regulatory Commission  
Washington, DC 20555

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Prepared as part of  
The Agreement on Research Participation and Technical Exchange  
under the International Thermal-Hydraulic Code Assessment  
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## ABSTRACT

Natural circulation experiments carried out in the REWET-III facility in 1985 have been used for RELAP5/MOD2 assessment. The REWET-III facility is a scaled-down model of VVER-410 type reactors. The facility consists of a pressure vessel in which the downcomer is simulated with an external pipe assembly, hot and cold legs with loop seals and a horizontal steam generator. The volume scaling factor compared to the reference reactor is 1:2333.

The present paper summarizes the experiences gained in the RELAP5/MOD2 calculations of selected REWET-III single- and two-phase natural circulation experiments. The code's ability to represent the main phenomena of experiments in both cases was satisfactory.

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## EXECUTIVE SUMMARY

Single- and two-phase natural circulation can play an important role as a passive heat removal mechanism in LWRs during transients and accidents. To investigate natural circulation phenomena in the primary circuit of the VVER-440-type pressurized water reactors in Loviisa, Finland, the REWET-III facility was built in 1985 by the Technical Research Centre of Finland and the Lappeenranta University of Technology.

One of the principal objectives of the experiments with this scaled facility was to generate a data base for the assessment of computer codes used to predict full-scale plant behaviour. The REWET-III facility is an electrically heated model of the Loviisa VVER-440 pressurized water reactor. The facility is scaled down with a scaling factor of 1:2333 by preserving the power to coolant volume ratio. The elevations are in scale 1:1 (except the reactor upper head). The facility consists of a model of the reactor vessel and one primary loop with loop seals and a horizontal steam generator. The primary loop represents to the five intact loops of the reference reactor. The heat transfer area of the tube bundle is scaled down with the above scaling factor 1:2333.

Two experiments have been chosen from the natural circulation experiment series as assessment case for the RELAP5/MOD2 cycle 36.04 code. The first experiment is a single-phase case at 20 kW thermal power corresponding to about 3 % decay heat level in the reference reactor. The second experiment is a two-phase case at 80 % water inventory and 30 kW thermal power of the facility. The main results of the experiments are the stationary final states into which the natural circulation process converges.

The nodalization of the REWET-III facility contains 64 volumes. The core nodalization is based on the chopped cosine power

distribution of the fuel rod simulators. The hot leg has been divided into nine relatively short volumes in order to allow a more precise prediction of steam flow in the two-phase case. The modelling of the horizontal steam generator has been one of the difficulties during the analysis. The horizontal steam generator has been divided into two horizontal pipe sections. The sections are placed one on top of the other. A vertical pipe component of three volumes is used to simulate the secondary side during the analysis. The nodalization used is capable of predicting both the distribution of flows on the primary side and, to some extent, the void distribution on the secondary side. On the other hand, the volumes on the secondary side have a very low L/D ratio which may cause numerical problems.

The form loss coefficients in the junction have caused numerous difficulties during the assessment. In the preliminary analysis, the code grossly overpredicted the primary mass flow in the single-phase calculation, but calculated the two-phase case reasonably well. Consequently, in the single-phase case the loss coefficients were chosen large enough to obtain the correct mass flow which in turn results in different coefficient values in the two cases.

After this choice, RELAP5/MOD2 succeeded in predicting the main parameters of the experiments, namely final pressures, mass flows and temperature distributions, reasonably well. The differences between the measured and calculated quantities are mostly within the error band of the measurements.

Comparison of the measured and calculated final states in REWET-III natural circulation experiments is given below.

	Pressure, MPa	Mass flow, kg/s
Single-phase: measured	0.68	0.08 ± 0.01
calculated	0.68	0.073
Two-phase: measured	0.45	0.17 ± 0.06
calculated	0.47	0.13

## 1 INTRODUCTION

The objective of this study is to assess the RELAP5/Mod2 cycle 36.04 code against natural circulation experiments performed with the REWET-III facility. The REWET-III facility is an 1:2333 volume scaled simulator of the Soviet VVER-440 type PWR, having one loop at the primary side and a horizontal steam generator. All the elevations (except the upper part of the upper plenum) in the facility match 1:1 with the reference reactor. The results of the experiments have been published in /1/

Two experiments have been used in the assessment process. The first one is a single-phase case at 20 kW thermal power, corresponding about 3 % decay heat level in the reference reactor. The second experiment is a two-phase flow case at 80 % filling ratio and 30 kW thermal power. The main goals of these experiments have been to recognize the various natural circulation modes in the facility and to determine the heat removal capability of the natural circulation process.

The main results of the experiments are the stationary final states into which the natural circulation process converges. The assessment has concentrated on an attempt to reproduce these final states as closely as possible, less attention has been paid to the transition behavior of the experiment. During the course of the analysis several interesting problems concerning the sensitivity of the code with respect to the requested time step have been detected.

In the following chapters the facility, the experiments, the model used and the results of the calculations will be described.



## 2 FACILITY AND TEST DESCRIPTION

### 2.1 THE REWET-III FACILITY

The REWET-III test facility /2/ is a rather comprehensive scaled model of the primary circuit of Loviisa NPP. It was mainly designed for investigations of natural circulation phenomena in VVER-440 reactors. The REWET-III facility is an extended version of the earlier REWET-II facility. The main design principle is the accurate simulation of the rod bundle geometry and the primary system elevations (Fig. 1). The reactor vessel is simulated by a stainless steel U-tube construction consisting down-comer, lower plenum, core and upper plenum.

All the elevations except the reactor upper head in the reactor vessel simulator are scaled to 1:1 (Fig. 2). The scale of the volumes and flow areas is 1:2333 referring to the number of the fuel rod simulators in the facility and the fuel rods in the reference reactor.

The simulation of the fuel-rod bundle consists of 19 indirectly electrically heated simulator rods. The heating coils are inside stainless steel claddings in magnesium oxide insulation. The heated length and the lattice pitch of the fuel-rod simulators as well as the number (= 10) and construction of the rod bundle spacers are the same as in the reference reactor. The characteristics of the rod bundle are presented in appendix A. The upper ends of the rods are attached to the upper tie plate (Fig. 3). The location of spacers are shown in Fig. 4. A schematic picture of the REWET-III facility are presented in Fig. 5 and the dimensions of pipes are given in Table 1.



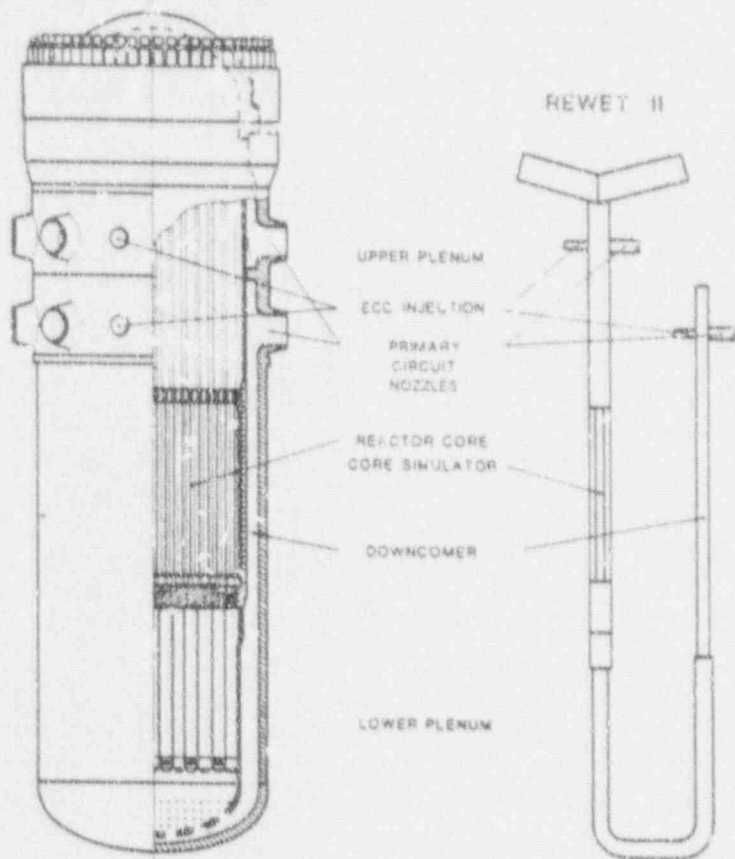


Fig. 1. Simulation of the VVER-440 reactor vessel by the REWET-III facility

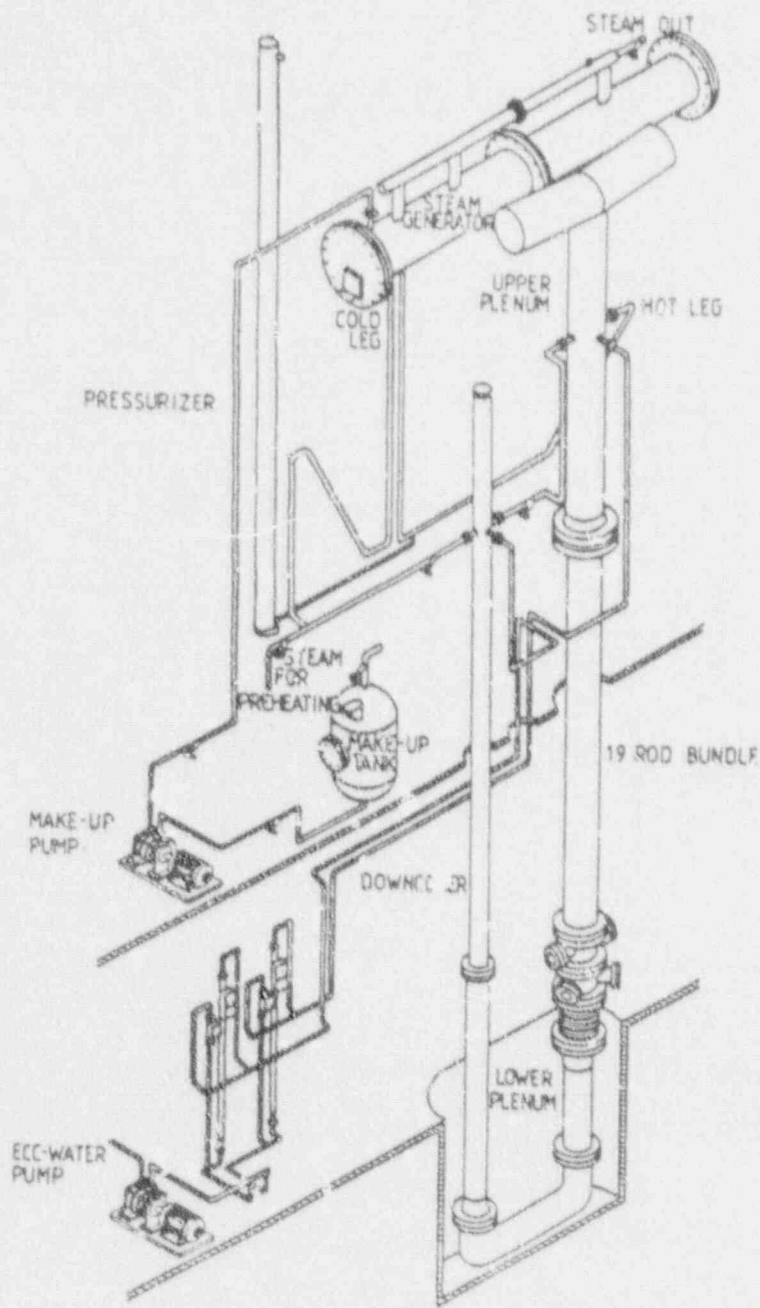


Fig. 2. REWET-III facility.

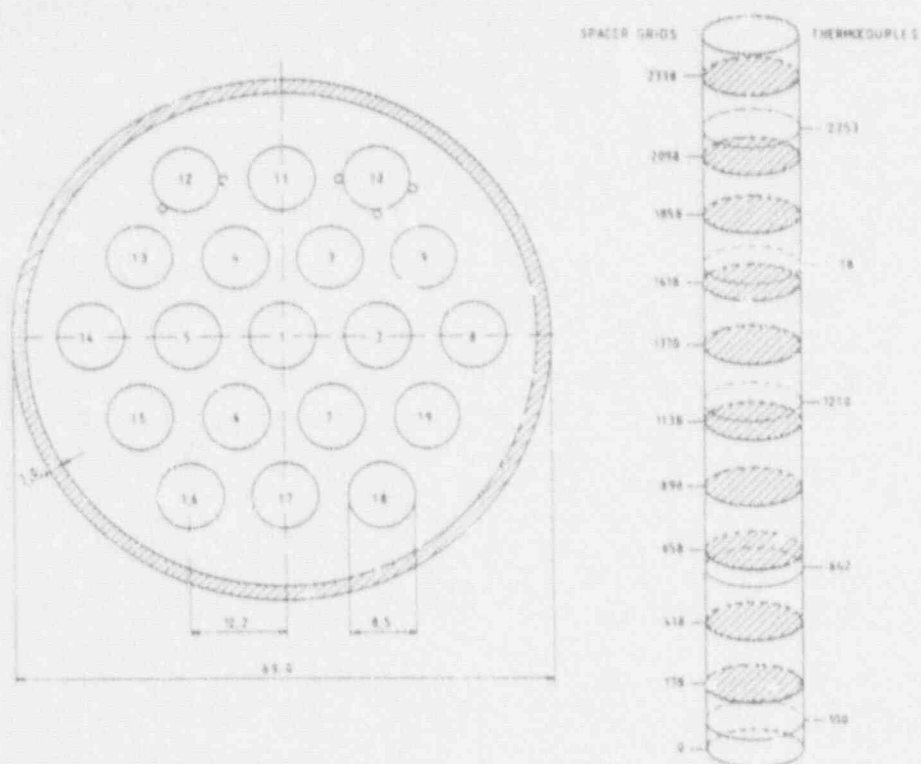


Fig. 3. Round rod bundle with rod simulators, (8,5 mm) and elevations of spacers.

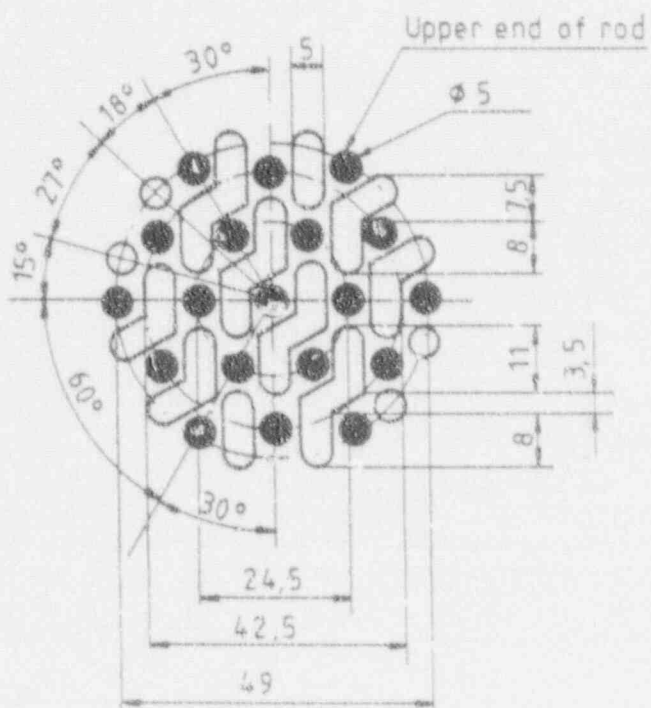


Fig. 4. Upper tie plate of REWET-II and REWET-III.

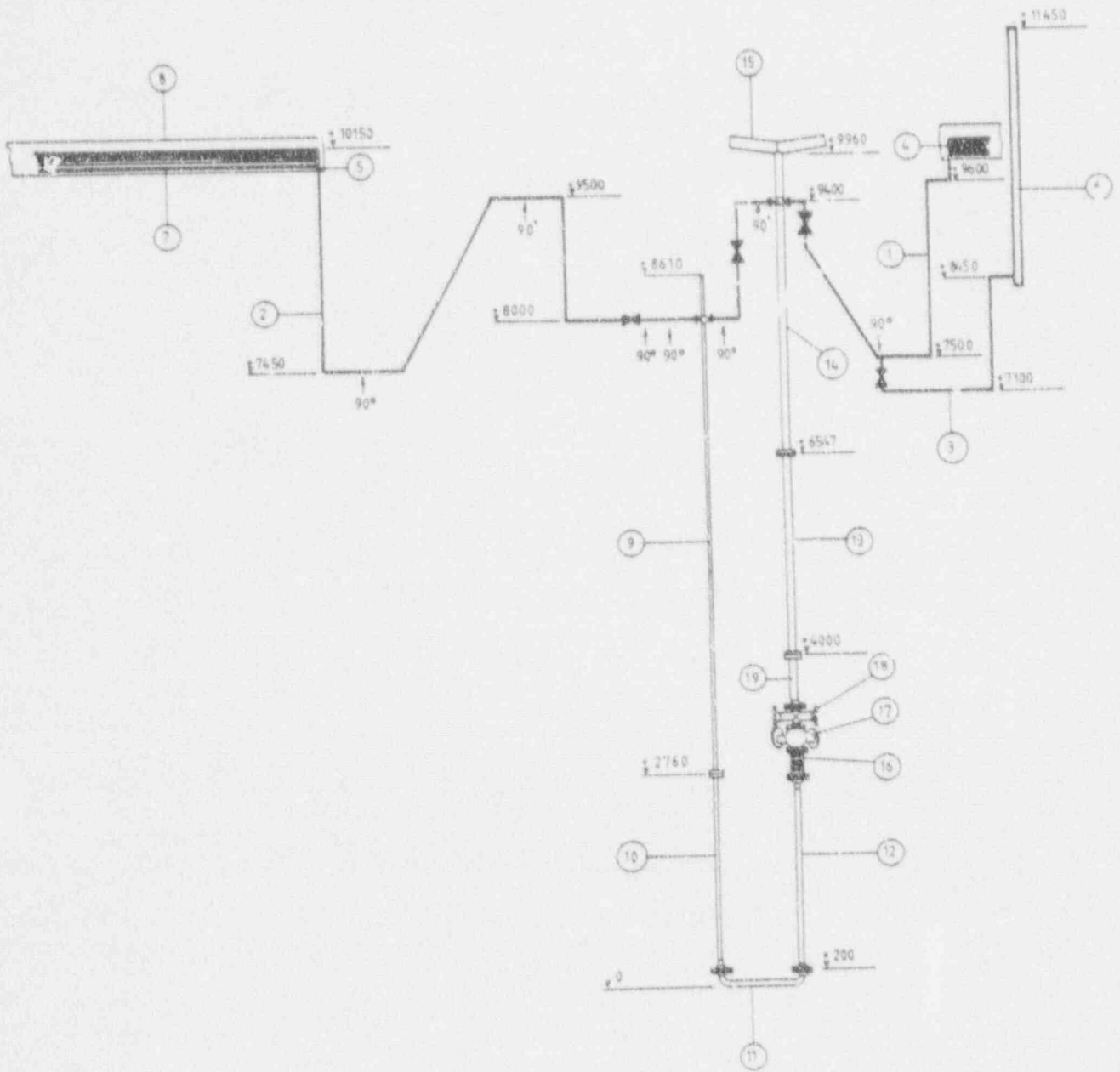


Fig. 5. Schematic picture of REWET-III facility.

Table 1. Pipe dimensions in REWET-III.

Name	Comments	Dimensions
1. Hot leg	5 x 90°, 1 x 30°	∅ 26.9 x 2.0 d <sub>i</sub> = 22.5 l = 5400
2. Cold leg	7 x 90°, 2 x 50°	∅ 26.9 x 2.0 d <sub>i</sub> = 22.9 l = 9670
3. Pressurizer line	3 x 90°	∅ 21.3 x 1.5 d <sub>i</sub> = 18.3 l = 3200
4. Hot leg SG collector (Cu)		∅ 54.0 x 1.5 d <sub>i</sub> = 51.0 l = 320
5. Cold leg SG collector (Cu)		∅ 54.0 x 1.5 d <sub>i</sub> = 51.0 l = 320
6. Pressurizer		∅ 70.0 x 2.0 d <sub>i</sub> = 66.0 l = 3100
7. SG-tubes (Cu)	(12 U-tubes)	∅ 15.0 x 1.0 d <sub>i</sub> = 13.0 l = 7674
8. SG		∅ 406.4 x 8.8 d <sub>i</sub> = 388.8 l = 4030
9. Downcomer	upper part	∅ 33.7 x 1.5 d <sub>i</sub> = 30.7 l = 5920
10. Downcomer	lower part	∅ 44.5 x 2.5 d <sub>i</sub> = 39.4 l = 2560
11. Lower plenum	horizontal	∅ 60.3 x 2.0 d <sub>i</sub> = 56.0 l = 740
12. Lower plenum	vertical	∅ 55.0 x 2.5 d <sub>i</sub> = 50.0 l = 2420
13. Core 1.	hexagonal shroud d <sub>hydr</sub> = 7.2 mm, s = 2mm, dist of opposite walls = 54.3,	l = 2547
13. Core 2.	round shroud d <sub>hydr</sub> = 14.1 mm	∅ 70.0 x 2.0 d <sub>i</sub> = 66.0 l = 2547
14. Upper plenum	vertical	∅ 69.0 x 2.0 d <sub>i</sub> = 67.0 l = 3540
15. Upper plenum	(7 x 400 mm)	∅ 88.9 x 2.5 d <sub>i</sub> = 83.9 l = 800
16. Bellow	(l = 184 - 244 mm)	- d <sub>i</sub> = 65.0 l = 240
17. Instrumentation nozzles.	Vol = 1.0 l	∅ 69.0 x 2.0 d <sub>i</sub> = 65.0 l = 200
18. Power wire nozzles.	Vol = 0.9 l	∅ 69.0 x 2.0 d <sub>i</sub> = 65.0 l = 190
19. Core inlet tube.	Vol = 1.6 l, d <sub>hydr</sub> = 11.1 mm	∅ 69.0 x 2.0 d <sub>i</sub> = 65.0 l = 750

The elevations of the loops correspond to the centerline of the loops of the reference reactor (Fig. 6). The horizontal steam generator simulator consists of 12 full length (7.7 m) horizontal U-tubes. The diameter of the U-tubes and the space between them are the same as in the reference reactor. The heat transfer area of the tube bundle is scaled down with the same scaling factor as the plena, and it corresponds to the total heat transfer area of the steam generators in the five intact loops of the reference reactor. In Fig. 7 the dimensions of the steam generator simulator are shown.



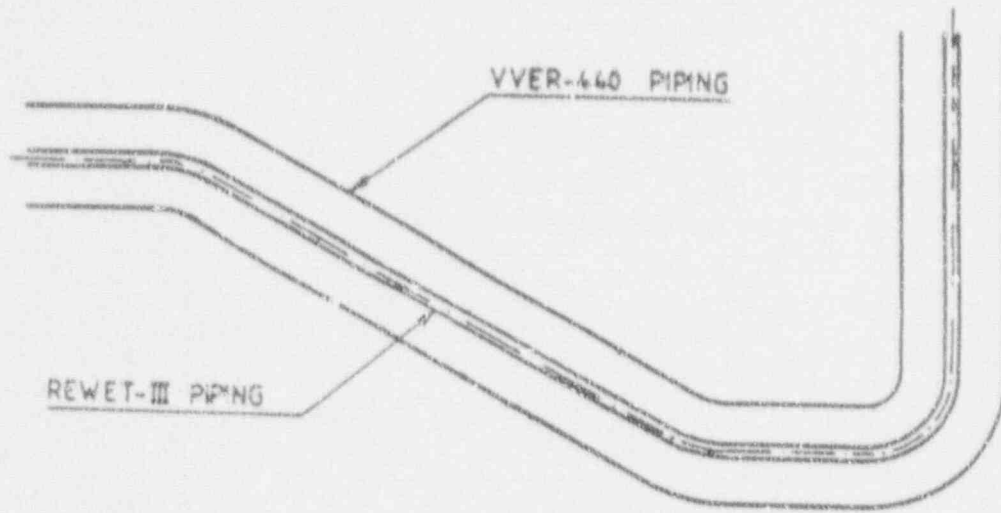


Fig. 6. REWET-III piping compared to VVER-440 piping.

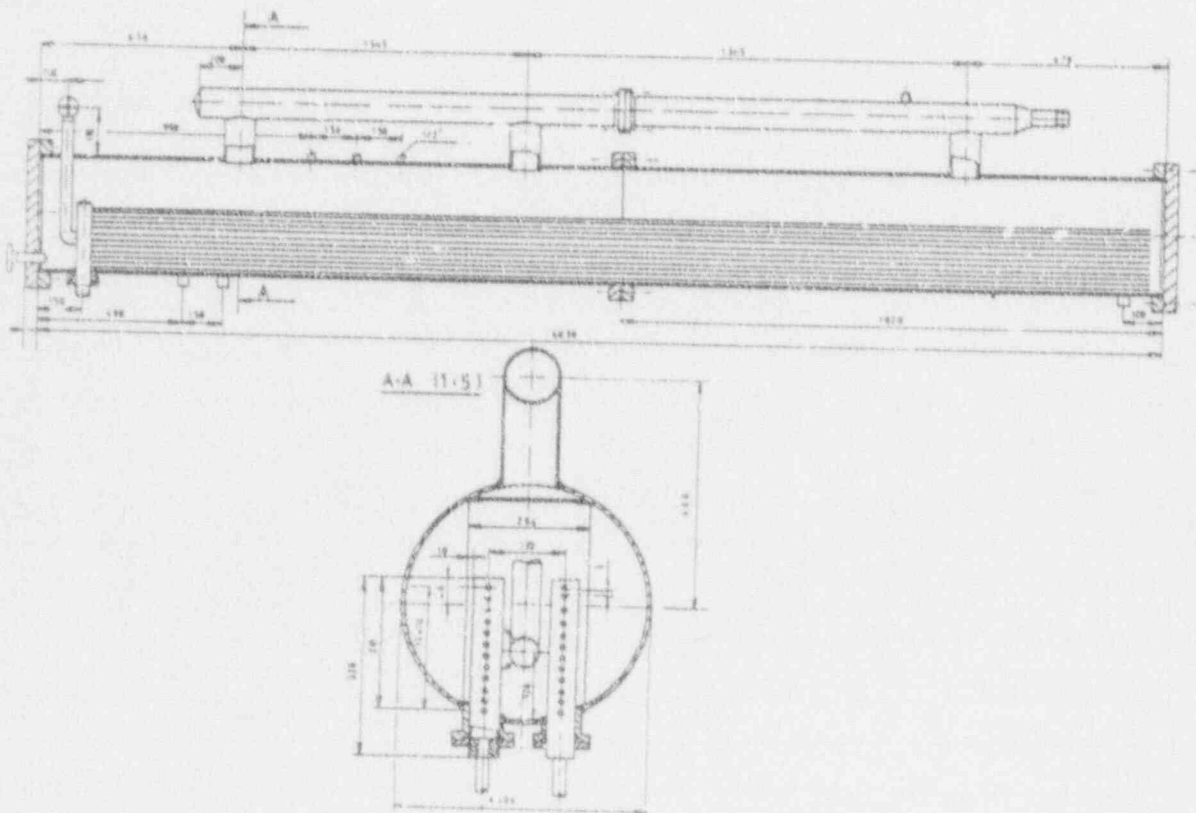


Fig. 7. REWET-III steam generator simulator.



## 2.2 Instrumentation and data acquisition system of the REWET-III facility

The main measurements in the experiments are coolant and rod cladding temperatures with thermocouples at different radial and axial locations. System pressure, pressure difference along the test section (core simulator), coolant flow rates and heating power are also measured. The primary and secondary fluid temperatures and the primary pipe temperature are measured from seven places in every second pipe in the steam generator. The measurement system is shown in Fig. 8 and the locations in Fig. 9. The data acquisition system consists of a measurement and control processor, a digital voltmeter and a desk-top computer (Fig. 10). The maximum speed to scan all 96 data channels during an experiment is once per second. With this speed it takes 10 minutes to collect a maximum of 58,800 readouts.

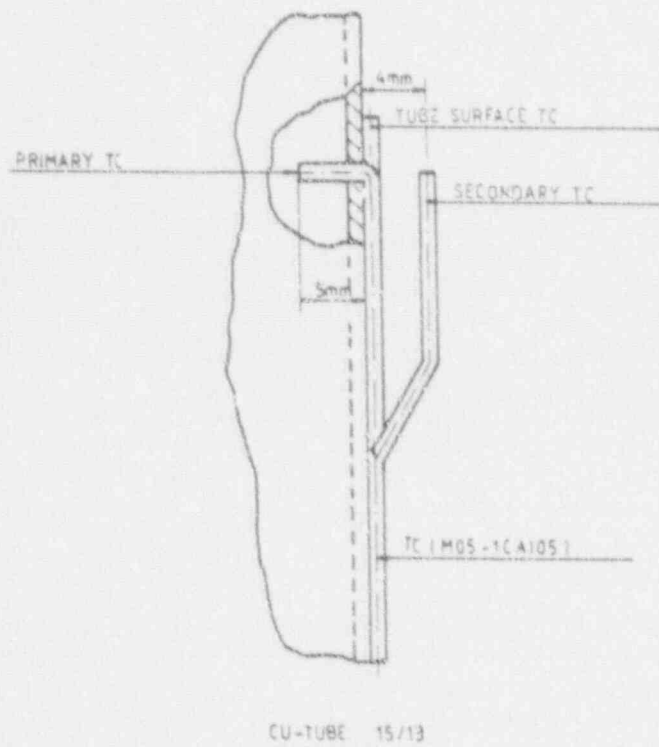


Fig. 8. SG tube thermocouple positions.

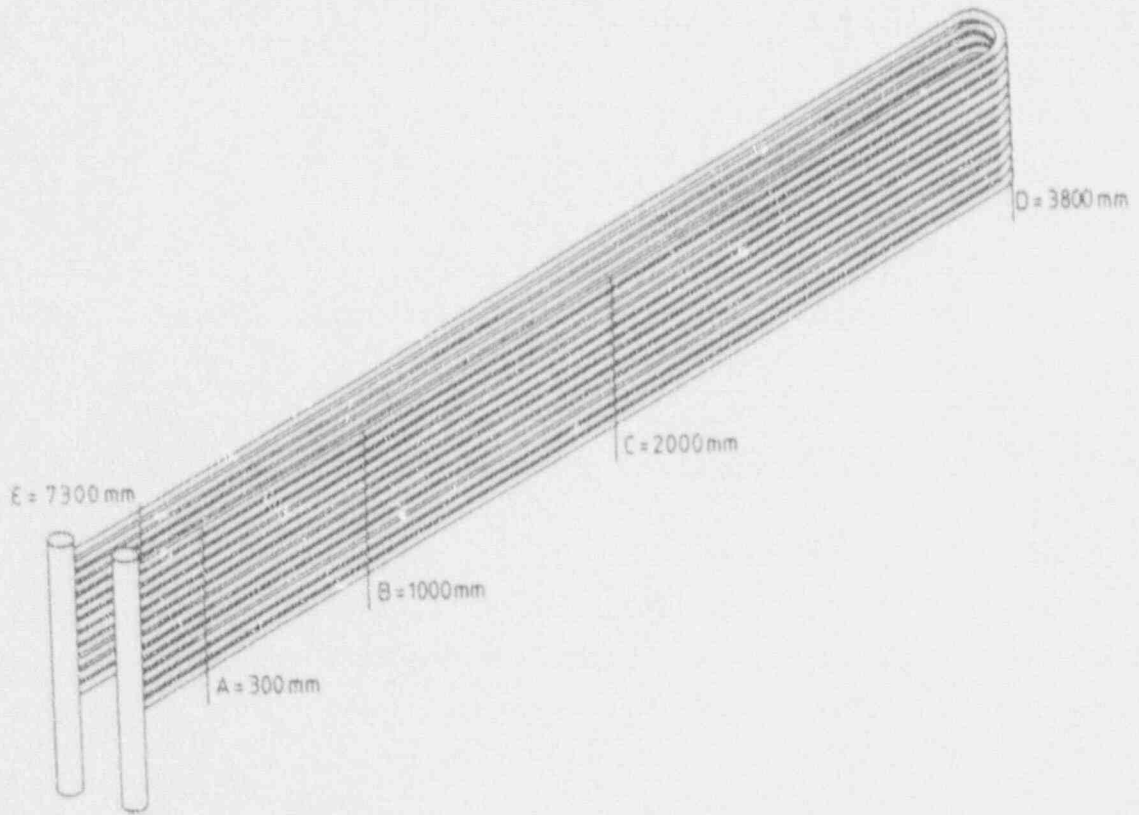


Fig. 9. SG thermocouple locations.

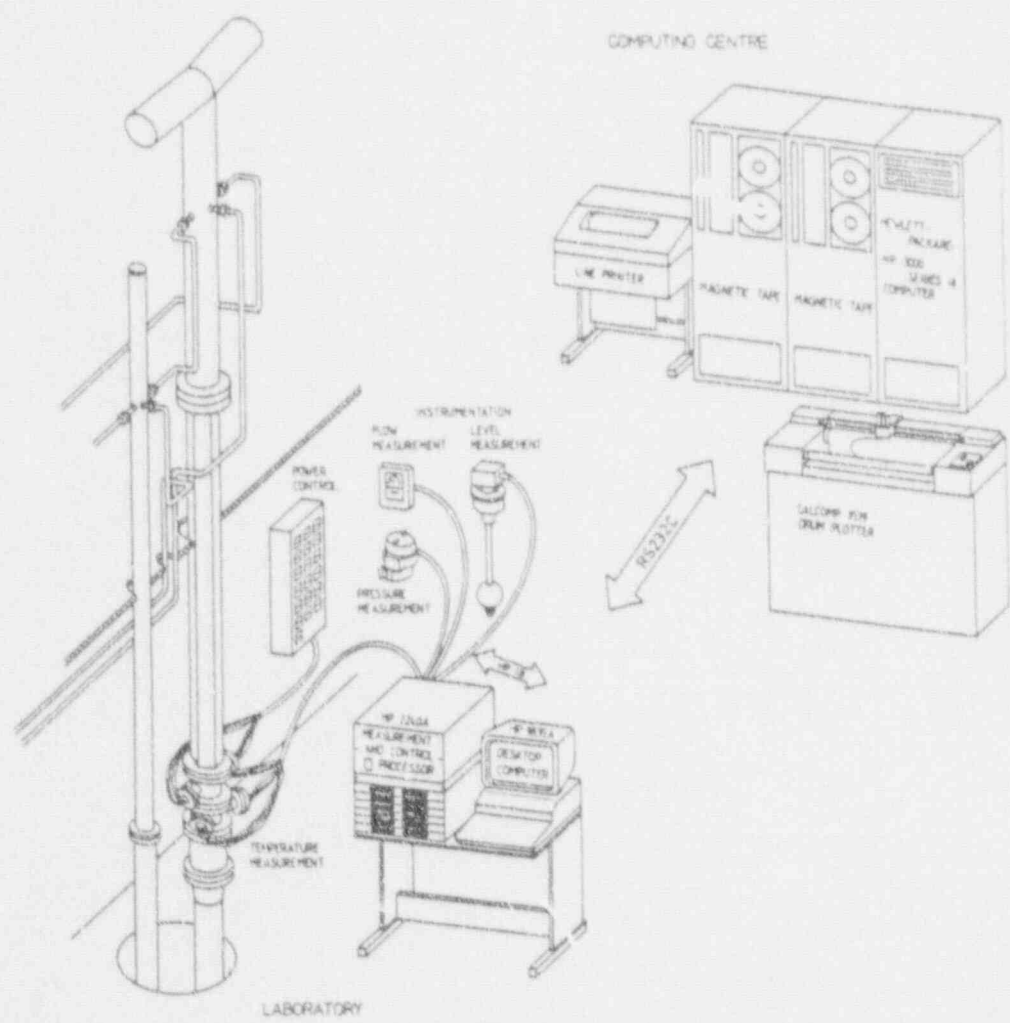


Fig. 10. REWET-III data acquisition system.

### 3. TEST CONDITIONS

A total of 22 experiments were made in this series. The principal objectives of the experiments were to characterize natural circulation phenomena under a variety of conditions and to generate a data base for computer codes used to predict full-scale plant behavior. The main parameters varied in the experiments were heating power, primary water inventory and noncondensable gas (air) content. The test matrix of the experiments is shown in Table 2.

Table 2. The REWET-III natural circulation experiments.

Number of the experiment	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	
Water Inventory	100 %	X	X																				
	90 %			X								X	X	X	X								
	80 %				X	X	X										X						
	70 %							X	X	X								X	X	X			
	65 %										X	X									X	X	X
	60 %											X	X										
Core power	30 kW					X			X					X					X				X
	20 kW		X		X			X			X		X			X		X		X			X
	15 kW	X		X	X			X			X		X			X		X		X			X
Noncondensable Gases Present												X	X	X	X	X	X	X	X	X	X	X	

Instead of regulating primary pressure during the experiments it was allowed to seek its equilibrium as a function of heating power and water inventory. The secondary side of the steam generators operated at saturated conditions and atmospheric pressure. The pressurizer was not used in the experiments (closed valve).

For the experiments the primary side of the facility was filled up and the heating up was performed at the fuel rod simulators at a low power level. The secondary side was heated to saturated condition by an electrical heating coil. While the temperatures and the pressure increased in the facility the required quantity

of water was depleted from the primary circuit. After that the heating power was adjusted to the specified level. The behavior of the facility was examined for 60 minutes from the moment the facility had reached the steady-state condition.

In the experiments with noncondensable gases the quantity of air required was left in the primary circuit (steam generator and/or upper plenum) during the filling up of the facility.

#### 4 CODE INPUT DESCRIPTION

The nodalization used in analyzing both of the experiments is shown in Fig. 11. The core nodalization is based on the chopped cosine power distribution of the fuel rods. Connection to the hot leg has been modelled using a crossflow junction. The hot leg (loop seal) has been divided into nine relatively short volumes in order to allow a more precise prediction of steam flow in the two-phase case. The horizontal steam generator has been divided into two horizontal pipe sections, each simulating six of the 12 U-tubes. The sections have been placed one on top of the other. A vertical pipe component of three volumes is used to simulate the secondary side. The top volume has a connection to time-dependent volume 260 that determines the boundary condition in the secondary side, which is the atmospheric pressure. The two other volumes have one section of primary tubing each. The hot and cold collectors have both been built of two stacked branches that have crossflow junctions to connect them into the U-tubes. The cold leg consists of relatively long volumes, especially in comparison with the cold collector, but this has not caused any problems. The connection to the downcomer is a crossflow junction, and the downcomer is a pipe of six volumes. The lower plenum has a connection to the boundary valve 300 and time-dependent volume 310, which were used to determine initial states of the system in both experiments and during the slow outflow transient at the beginning of the two-phase calculation.

A reasonable modelling of the horizontal steam generator has been one of the most difficult tasks during this analysis. The model described here is capable of predicting both the void distribution on the secondary side and the distribution of flows on the primary side. Similar nodalization has been used to analyze the behavior of the steam generators of an actual plant /3/. On the other hand, it has at least two drawbacks: the volumes on the secondary side have a very low length to diameter (L/D) ratio, which in turn may have caused some numerical problems, and the uneven distribution of primary side volumes within the pipe components cause a slightly distorted distribution of heat transfer from primary to secondary side.



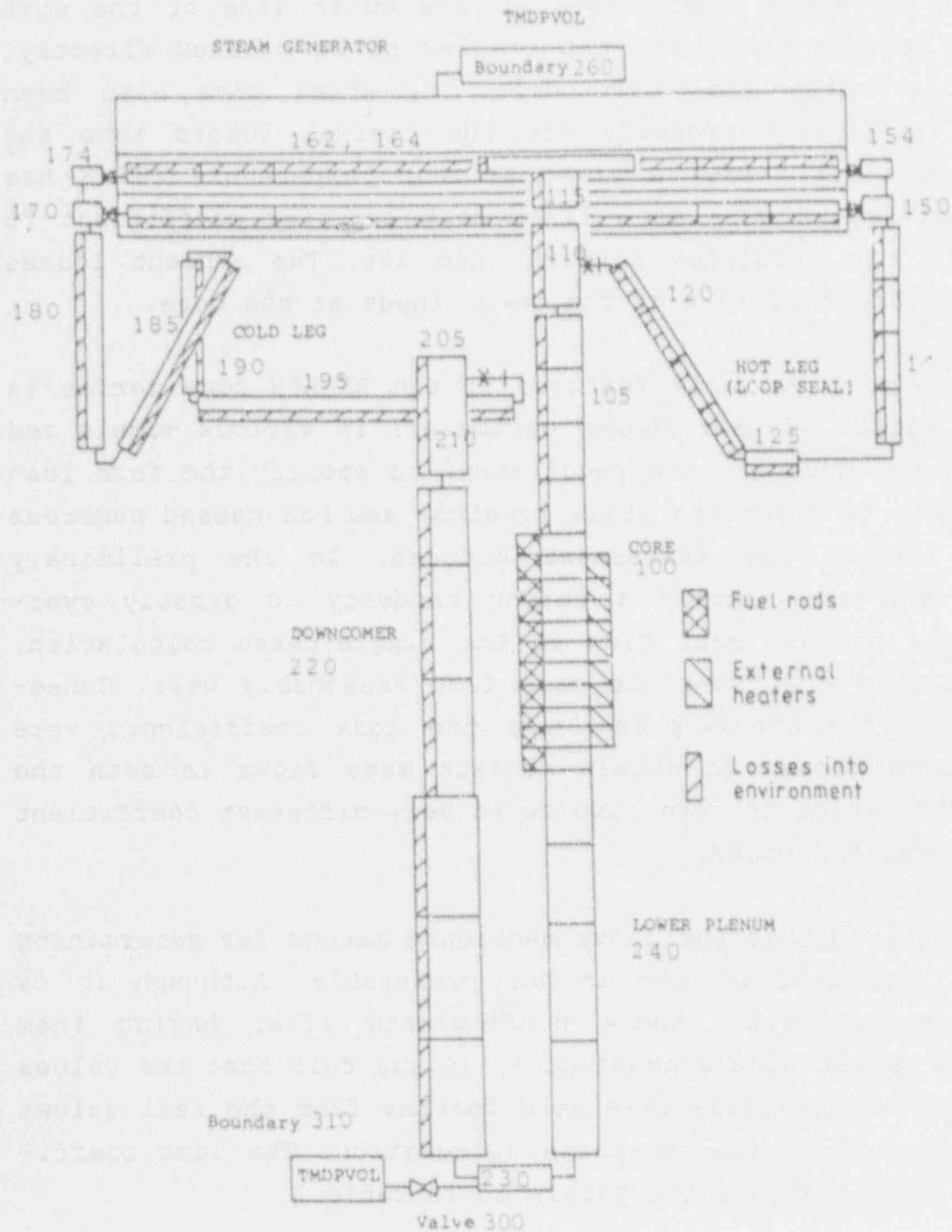


Fig. 11. The nodalization of REWET-III facility for RELAP5/Mod2 Natural Circulation Analysis.

The fuel rods have been modeled using cylindrical heat structures with appropriate attention being paid to both axial and radial power distribution. The external heaters have been described as fixed heat fluxes on the outer side of the core housing, because they were too complex to be modeled directly. The piping walls and surrounding insulators have also been modeled to account properly for the thermal losses into the environment. For these, a fixed ambient temperature 293 K has been specified as well as a fixed heat transfer coefficient 26 W/m<sup>2</sup>K from the insulator surface into air. The ambient losses are of the order of 10 % of the power input at the core.

One of the most valuable features of the RELAP5 code series is the elimination of user-chosen parameters in various models and correlations. However, the requirement to specify the form loss coefficients in junctions still remains, and has caused numerous problems during the assessment process. In the preliminary analysis the code showed a strong tendency to grossly over-predict the primary mass flow in the single-phase calculation, but calculated the two-phase mass flow reasonably well. Consequently, in the single-phase case the loss coefficients were chosen large enough to obtain correct mass flows in both the experiments, which in turn results in very different coefficient values in the two cases.

It is recognized that the above mentioned method for determining the flow loss coefficients is not preferable. Although it is better not to adjust these coefficients after having them determined on the single-phase data, it was felt that the values used in the single-phase case were farther from the real values than those used in the two-phase calculation. The loss coefficients of both analyses are tabulated in Table 3.

Table 3. Primary loop form loss coefficients in the REWET-III natural circulation analyses with RELAP5/Mod2.

Junction	Location	Single-phase		Two-phase	
		Forward	Backward	Forward	Backward
100-01 to 10	core	4.81	4.81	0.41	0.41
102	core to upp. ple.	7.9	7.9	1.9	1.9
105-01 to 03	upp. ple., lower	3.22	3.22	0.0	0.0
110-01	u.p. low to conx	3.26	3.26	0.66	0.66
110-02	conx to hot leg	6.22	6.22	1.22	1.22
110-03	conx u.p. upper	3.25	3.25	0.85	0.85
115-01	upp. ple. up	5.16	5.16	0.16	0.16
120-01 to 03	hot leg 1	1.9	1.9	0.0	0.0
125-01,02	loop seal bottom	3.25	3.25	0.36	0.36
140-01 to 03	hot leg 2	3.22	3.22	0.0	0.0
150-01	hot leg to SG coll	5.5	6.1	2.5	3.1
150-02	SG coll to low U-tb	8.7	4.1	3.7	2.1
150-03	to upper collector	7.9	5.3	1.3	1.3
154-01	upp. coll to up U-tb	17.9	13.0	3.7	2.1
162-01,02	SG low tubes begin	0.7	0.7	0.0	0.0
162-03	U-bend, SG low tb	2.11	2.11	0.11	0.11
162-04,05	SG low tubes end	0.7	0.7	0.0	0.0
164-01,02	SG upp tubes begin	0.7	0.7	0.0	0.0
164-03	U-bend, SG upp tb	2.11	2.11	0.11	0.11
164-04,05	SG upp tubes end	0.7	0.7	0.0	0.0
174-01	upp. tb to coll	11.0	13.9	2.3	4.1
170-01	SG coll to cold leg	6.1	4.5	3.1	2.5
170-02	low tubes to coll	4.1	8.7	2.3	4.1
170-03	from upp coll	7.3	7.9	1.3	1.3
183	cold leg loop seal	9.6	9.6	0.6	0.6
187	cold leg top	9.6	9.6	0.6	0.6
193	cold leg flat	9.6	9.6	0.6	0.6
210-01	cold leg to downc	11.82	11.82	1.42	1.42
210-02	downcomer	9.94	9.94	0.94	0.94
220-01 to 05	downcomer	1.1	1.1	0.0	0.0
230-01	downc to low ple.	14.89	14.89	0.89	0.89
230-02	lower plenum	14.29	14.29	0.89	0.89
240-01	lower plenum	18.63	18.63	0.63	0.63
240-02,03	lower plenum	27.63	27.63	3.63	3.63
245	low ple to core	16.87	16.87	0.87	1.87

The initial conditions of the single-phase case were chosen to match the final state as closely as possible. To facilitate this search the boundary 310 was set to a fixed pressure 0.74 MPa, corresponding to the measured final pressure 0.65 MPa at the primary pressure measurement location. The temperature (the specific internal energy) of volume 310 was set to follow volume 220-06. Because a closed water-filled loop is very stiff against even minor fluctuations of the energy balance due to the extremely small compressibility of water, a small bubble of air was left into the upper part of the upper plenum to smoothen the pressure variations while the system was on the way to the steady final state. The presence of such a bubble is justified, because ordinary tap water was used in the experiments and some of the dissolved air will be released during the test.

The steady-state search algorithm of RELAP5/Mod2 proved to be almost useless, because it predicted the existence of a steady state in most calculations too early, i.e. while the system was still changing (although relatively slowly). In this case an algorithm based on setting the time derivatives zero would most probably have yielded more reasonable results in much less time and with less effort.

In the two-phase case the calculation was started with a stable single-phase natural circulation at about 0.3 MPa pressure and 12 kW heating power. The air bubble in the upper plenum had to be removed because of a number of code failures during the initial state search. All of these failures were caused by steam property table overflows and occurred in volumes that were almost completely filled with air, with very small amounts of steam and water still present. The volumes that caused these failures also had heat structures representing pipe walls connected to them.

The transient part of the two-phase case was initiated by lifting the core power to 28 kW (the missing 2 kW were assumed to leak from the external heaters of the core directly at the surroundings), setting the primary boundary 310 at atmospheric pressure and opening valve 300. The mass flow rate through this valve was about 0.03 kg/s, which was slightly less than the

upper limit of the outlet flow in the experiment. The valve was closed when the integrated mass flow through it reached a preset value, 8 kg, which corresponds to the 80 % filling ratio with sufficient accuracy. The final state was the steady state into which the primary circuit converged after closing the valve.

Both of these calculations are sensitive to the initial thermodynamic state of the system. This is obvious from the fact that the solution of the system equations in the primary side is bounded only by the heat transfer from or to the walls (except during the short outflow period in the beginning of the two-phase case).

## 5 RESULTS

RELAP5/Mod2 succeeded in predicting the main parameters of the experiment, namely final pressures, mass flows and temperature distributions, very well. Some small differences between measured and calculated quantities can be found, but they are usually within the error band of the measurement.

The final pressures and mass flows of both calculations are compared to those of the experiments in Table 4 and the measured and calculated temperature distributions are shown in Figs. 12 and 13.

Table 4. Comparison of measured and calculated (in brackets) final states of the REWET-III natural circulation tests.

	Pressure, MPa	Mass flow, kg/s
Single-phase	0.68 (0.68)	0.08±0.01 (0.073)
Two-phase	0.45 (0.47)	0.17±0.06 (0.13)



The single-phase experiment shows relatively large mass flow oscillations that could not be reproduced. In the two-phase case both measured and calculated mass flows oscillate quite strongly, but in the calculations the oscillations die out much faster. These oscillations have far too small frequency to be of a numerical origin. In the both cases the final state is sensitive to the ambient losses and the form loss coefficients. If the ambient losses from the hot leg are neglected, the oscillations have considerably larger amplitude and survive much longer (see Appendix B).

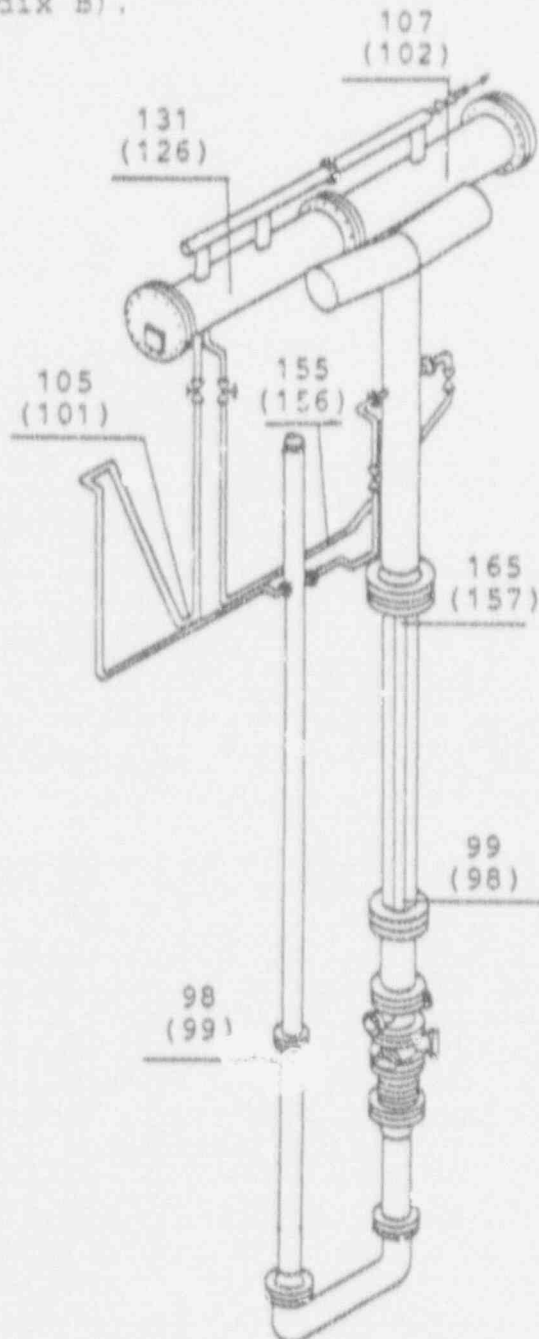


Fig. 12. Measured and calculated (in brackets) temperature in the steady single-phase natural circulation.



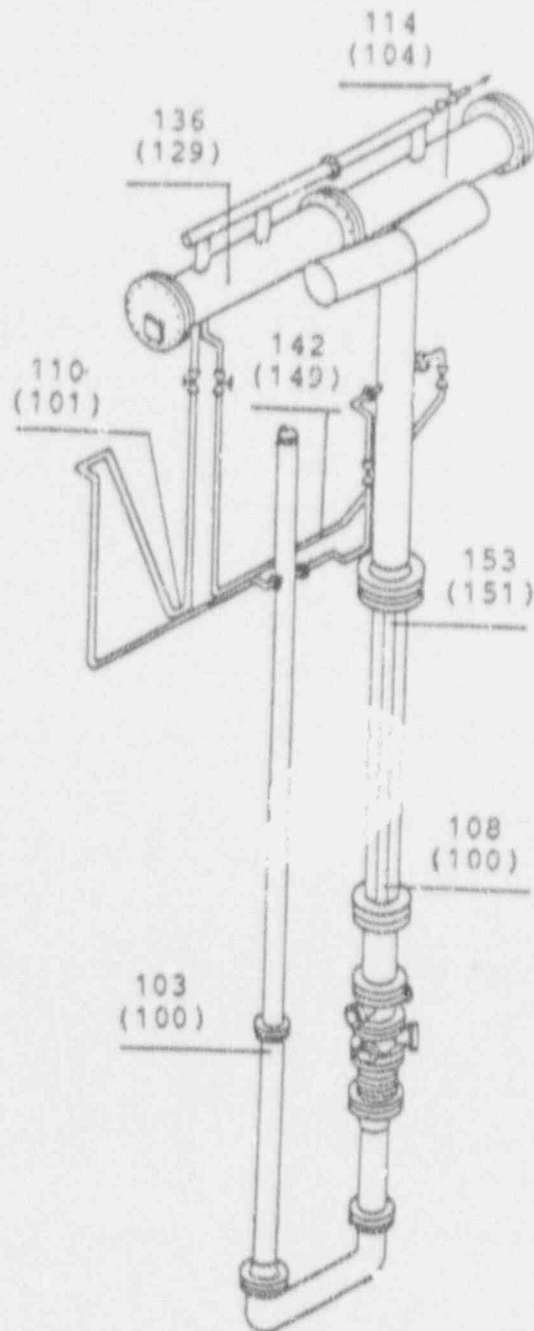


Fig. 13. Measured and calculated (in brackets) temperatures in steady two-phase natural circulation.

The steam generator secondary side starts to show unstable characteristics even at maximum requested time steps clearly below the Courant limit (Fig. 14). The vast majority of minimum Courant limits gathered into the second volume of the steam generator.



Fig. 14. Steam generator hydrodynamic instability appears when the requested time step is increased from 0.25 to 1.0 s. The Courant limit is about 0.7 s, and the code immediately resets the time step to 0.5 s.

The solution of the system equations in the steam generator secondary side remains stable when the requested time step is shortened to  $1/3 \dots 1/4$  of the Courant limit. This is obviously due to the relatively low L/D value of the secondary side volumes, and has also to do with the stability of wall to fluid heat transfer, which is not controlled in the code at all.

The run statistics in the single-phase case show that when 0.2 s is used as the maximum time step, the CPU consumption is 0.00578 s per volume per time step. 1568 time steps were required to simulate 312.8 seconds of experiment, and the time step

had to be reduced only twice. The Courant limit in the single-phase case is 0.56 s. In the two-phase case 10181 time steps were used to simulate 999 s of transient. The requested time step was 0.1 s, Courant limit 0.44 s and 63 time step reductions took place. The CPU consumption was 0.00586 seconds per volume per time step.

During the analysis of the two-phase case it soon turned out that the bubbles condense on the pipe walls, and saturated liquid passes through the loop seal. As the liquid rises towards the steam generator collector, hydrostatic pressure may sometimes decrease sufficiently to allow some evaporation to take place (Fig. 15).

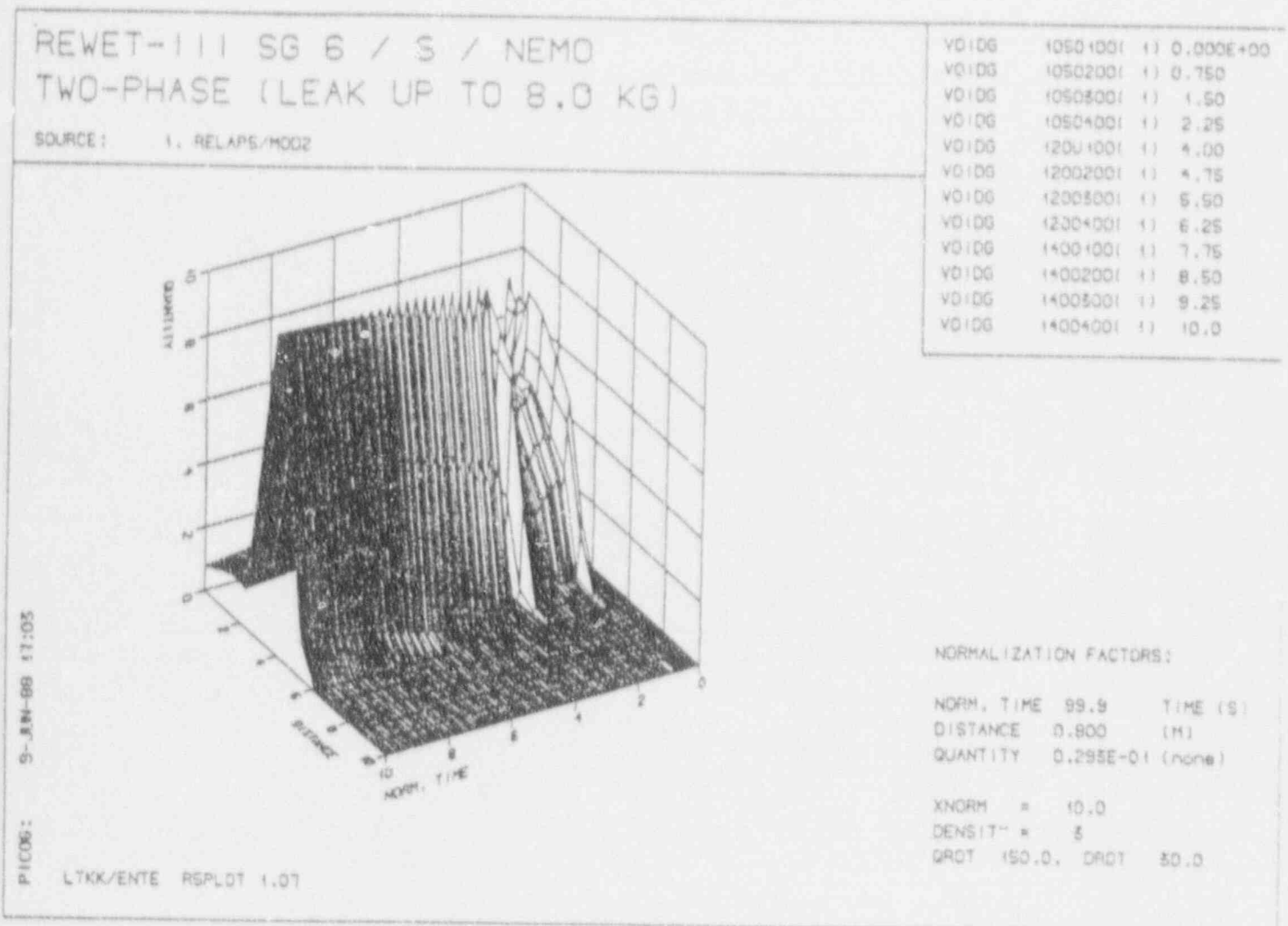


Fig. 15. Steam void fraction distribution in the hot leg.

## 6. CONCLUSIONS

The calculations show that RELAP5/Mod2 is capable of calculating natural circulation phenomena satisfactorily also in facilities with horizontal steam generators and thus relatively low gravity head. However, several shortcomings of the code were observed.

To model the natural circulation phenomena one must know the pressure losses in various part of the facility accurately. The amount of heat lost into environment has a very strong effect on the result, too.

It was observed during the analysis that volumes with small L/D ratio, such as those used to model the steam generator secondary side in the REWET-III facility, show unstable behaviour at time steps considerably smaller than the Courant limit. In this case the stable results required setting the maximum time step to one fourth to one third of the Courant limit.

A number of code failures were observed, when an air bubble was let to travel along the hot leg. These failures were caused by steam table overflows which occurred in a volume filled with air, with only small quantities of water or steam being present. It is suggested that the non-condensable gas model be improved to handle this type of situation properly.

The steady state search algorithm was found to be insufficient. In these experiments most quantities change relatively slowly, and the algorithm predicted the existence of a steady state too early, while the thermodynamic state still undergoing a change. Although the benefits of the current algorithm are recognized, it is suggested that an additional algorithm will be added to the code. This additional steady state algorithm could be based on setting the time derivatives in all equations to zero.

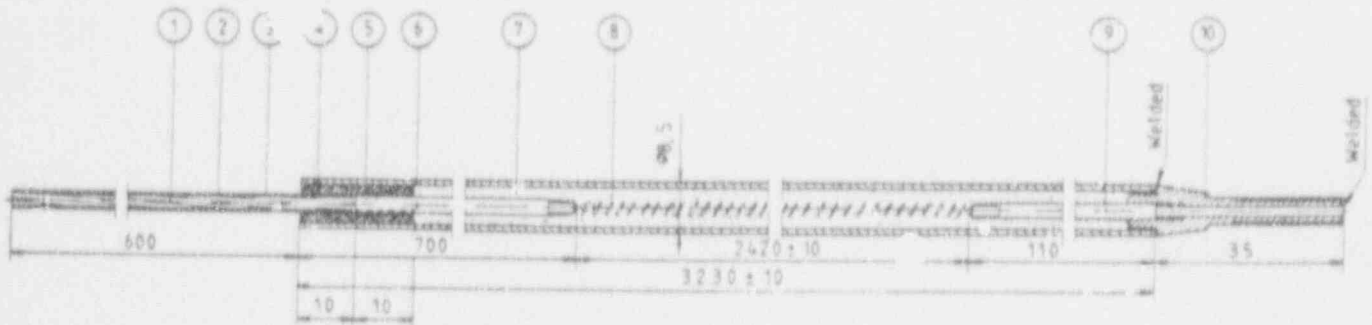
The fact that the steam bubbles do not penetrate the hot leg loop seal requires an explanation. A large number of more thorough analyses with various filling ratios and modified nodalizations may be needed to further examine this phenomenon.



## REFERENCES

1. T. Kervinen, O. Hongisto, Natural Circulation Experiments in the REWET-III Facility. ANS/ENS Topical Meeting on Thermal Reactor Safety, San Diego 2-6.2.1988.
2. T. Kervinen, H. Purhonen, T. Haapalehto, Description of REWET-II and REWET-III Facilities. Technical Research Centre of Finland, Espoo. Research Note 929, 1989.
3. Ismo Karppinen, Nodalization of a horizontal steam generator by the RELAP-5 code. Diploma Thesis, Helsinki University of Technology, 1987.

## APPENDIX A



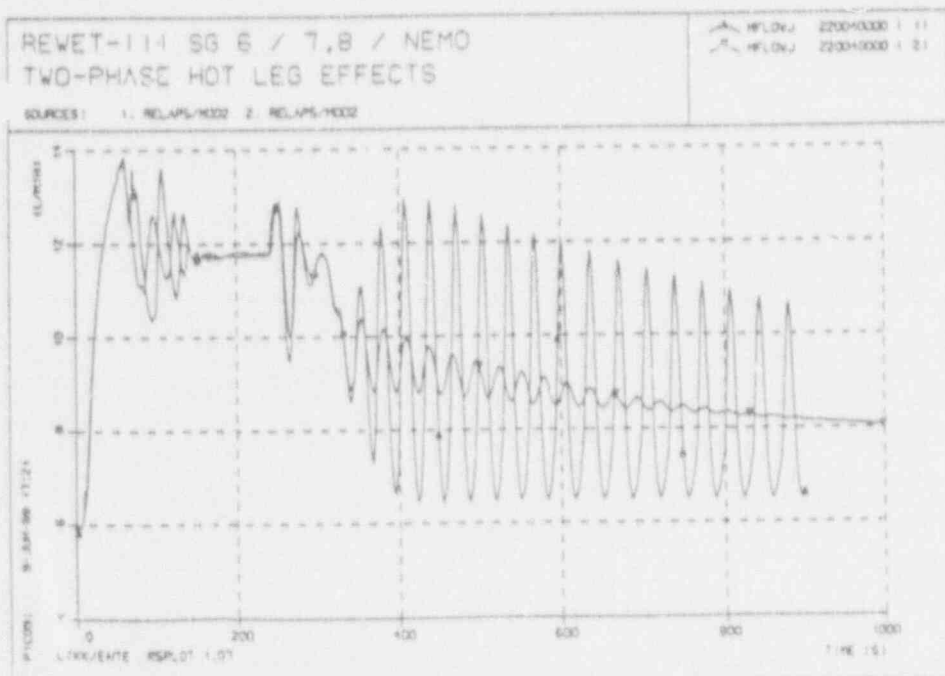
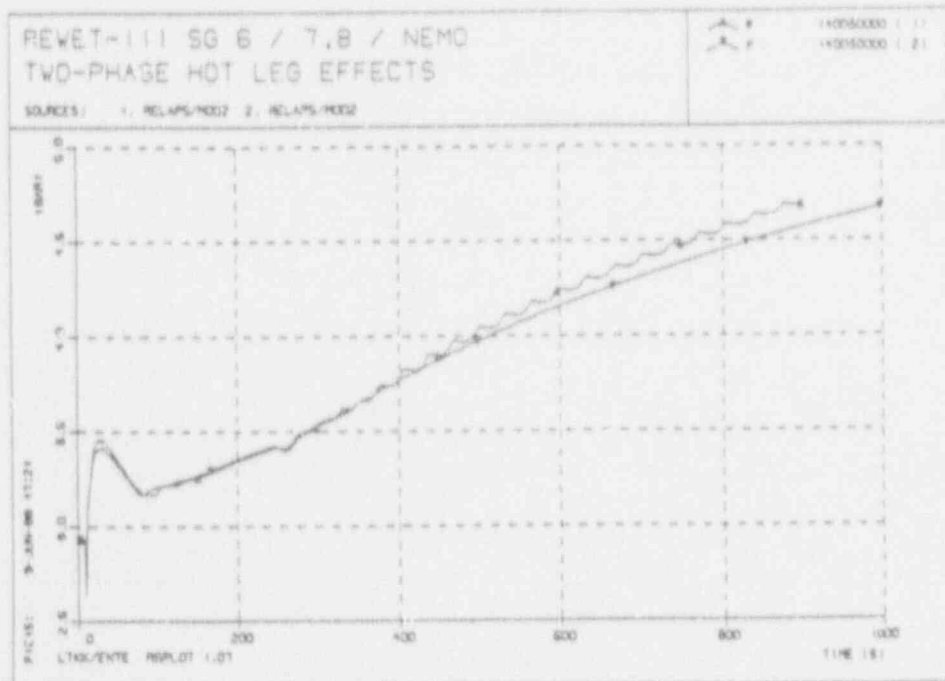
10	Top boss	AISI 304
9	Conduct. pin	5137k/h11
8	Heating element	Cr
7	MgO	
6	Cladding	AISI 316L
5	Conductor pin	5137k/h11
4	Silicone filling	Rhod-sil-cof1Fluide
3	Shrink-on plastic tube	d = 0.4
2	Shrink-on plastic tube	d = 3.2
1	Lead wire	Cu 1.2 mm <sup>2</sup>

LOVAL

Fuel rod simulator (Ø8.5)

## APPENDIX B. The effect of ambient thermal losses

The two figures below show the primary pressure and mass flow respectively during two-phase natural circulation. The strongly oscillating curves marked with  $\Delta$  were obtained when the conduction losses from the hot leg were not modeled (that is, they were assumed zero). The smoother curves with marker  $\nabla$  were obtained when the hot leg losses were included in the calculation. Losses from other parts of the system were equal in both cases.



APPENDIX C      LISTING OF INPUT DATA FOR SINGLE PHASE CASE

\* REWET-III NATURAL CIRCULATION, SG 2 FINAL /8/ L16-5 / JUHANI HYVARINEN

\* ---- MOD2 VERSION ----

\* FILLING RATIO 100 % AND POWER 14+5 GW = THE APPROXIMATE FINAL STATE  
\* PRESSURE ABOUT 6.6 BAR

100 NEW TRANSNT

101 RUN

102 SI SI

\* CPU-REMAINING CARD

105 5.0 10.0

\* HYDRODYNAMIC SYSTEM CARDS

	REF. VOLUME	REF. ELEVATION	FLUID	SYSTEM NAME
120	230010000	0.0	WATER	PRIMARY
121	250010000	9.5	WATER	SECONDRY

\* TIME STEP CONTROL CARD(S)

\* OPTION ssd03: ss= 7 = 4+2+1 = OMIT

\* -SECOND BLOCKS OF VOL&JUN DATA

\* -HEAT STRUCTURE TEMPRATURES

\* d = 2 \* OBTAIN MINOR ELITS AT EVERY HYDRODYNAMIC  
\* TIME STEP

*201	10.0	0.5E-6	0.8	00003	1	100	3000
*203	600.0	0.5E-6	0.6666666666	00003	3	450	3000
*202	99.0	0.5E-6	0.2	00003	5	1200	3000
203	300.0	0.5E-6	0.2	00003	5	1500	3000

\* TRIPS

\* TRIP FROM SG INLET PRESSURE  $\geq$  2.0 MPA (20 BAR) OR  $\leq$  0.20 MPA

	VARIABLE	OF VOLUME	RELATION	2ND VAR	OF 2ND VOL	+CONST	NOT LATCHED
501	P	140030000	GE	NULL	0	2.00E6	N
502	P	140030000	LE	NULL	0	0.20E6	N

\* TRIP TO STOP NEAR THE STEADY STATE

*503	MFLOWJ	300000000	LT	NULL	0	1.0E-4	N
*504	TIME	0	GT	NULL	0	150.0	L

\* LOGICAL TRIP(S)

601	501	OR	502	N
*602	503	AND	504	N

\* TRANSIENT TERMINATING TRIP(S)

600 601



\*  
\* MINOR EDIT REQUESTS:

\* TEMPERATURES

\*  
301 TEMPF 100010000  
302 TEMPF 100110000  
303 TEMPF 125010000  
304 TEMPF 150010000  
305 TEMPF 162010000  
306 TEMPF 162020000  
307 TEMPF 162040000  
308 TEMPF 162050000  
307 TEMPF 162060000  
308 TEMPF 164010000  
309 TEMPF 164020000  
310 TEMPF 164040000  
311 TEMPF 164050000  
312 TEMPF 164060000  
313 TEMPF 170010000  
314 TEMPF 180010000  
315 TEMPF 250010000  
316 TEMPF 250020000  
317 TEMPF 250030000

\* HEAT INPUTS IN CORE

\*  
320 Q 100010000  
321 Q 100020000  
322 Q 100030000  
323 Q 100040000  
324 Q 100050000  
325 Q 100060000  
326 Q 100070000  
327 Q 100080000  
328 Q 100090000  
329 Q 100100000  
330 Q 100110000

\* MASS FLOWS

\*  
332 MFLOWJ 102000000  
333 MFLOWJ 162020000  
334 MFLOWJ 164020000  
335 MFLOWJ 220040000  
\*336 MFLOWJ 300000000

\* VELOCITIES

\*  
\*349 VELFJ 256000000  
\*350 VELGJ 256000000

\* PRESSURES

\*  
337 P 140030000  
338 P 100110000  
339 P 250030000

\* SOME HEAT STRUCTURE TEMPERATURES AT SG TUBES

\*  
\*354 HTEMP 162100103  
\*355 HTEMP 162100603  
\*356 HTEMP 164100103  
\*357 HTEMP 164100603

\* HEAT INPUT RATES AT SG TUBES

```

*
340 Q 162010000
341 Q 162020000
342 Q 162030000
343 Q 162040000
344 Q 162050000
345 Q 162060000
*
346 Q 164010000
347 Q 164020000
348 Q 164030000
349 Q 164040000
350 Q 164050000
351 Q 164060000
*
* STEAM VOID FRACTIONS
*
353 VOIDG 250010000
354 VOIDG 250020000
355 VOIDG 250030000
*
356 VOIDG 115010000
357 VOIDG 115020000
*
358 QVALA 115020000
*
* CONTROL VARIABLES (DPS, EXCESS STEAM GENERATION, HEAT INPUTS)
*
385 CNTRLVAR 1
386 CNTRLVAR 2
387 CNTRLVAR 3
388 CNTRLVAR 4
389 CNTRLVAR 7
390 CNTRLVAR 20
391 CNTRLVAR 21
392 CNTRLVAR 22
393 CNTRLVAR 23
394 CNTRLVAR 24
395 CNTRLVAR 25
396 CNTRLVAR 26
397 CNTRLVAR 27
398 CNTRLVAR 28
*
* SPECIALITIES
*
399 CPUTIME 0
*
*-----*
* CONTROL VARIABLES
*-----*
* PRESSURE DIFFERENCES:
* DP = A0 + A1*VAR1 + A2*VAR2. DIMENSIONS NOT SCALED (SCALE=1.0)
*
* -- OVER CORE
*
* NAME TYPE SCALE INIT.VAL INIT.FLG=COMPUTE NO LIMITS
20500100 DPCORE SUM 1.0 0.0 1 0
* A0 A1 VAR1 CODE VOL1 CODE
* + A2 VAR2 VOL2
20500101 0.0 1.0 P 100010000 * CORE BOTTOM
+ -1.0 P 100110000 * CORE TOP
*
* -- OVER HOT LEG
*

```

	NAME	TYPE	SCALE	INIT.VAL	INIT.FLG=	COMPUTE	NO	LIMITS
20500200	DPHTLEG	SUM	1.0	0.0		1		0
*	A0	A1	VARI CODE	VOL1 CODE	+		A2,VAR2,VOL2	
20500201	0.0	-1.0	P	150010000	*		HOT LEG COLLECTOR	
+		1.0	P	230010000	*		LOWER PLENUM	
*	- OVER COLD LEG							
	NAME	TYPE	SCALE	INIT.VAL	INIT.FLG=	COMPUTE	NO	LIMITS
20500300	DPCDLEG	SUM	1.0	0.0		1		0
*	A0	A1	VARI CODE	VOL1 CODE	+		A2,VAR2,VOL2	
20500301	0.0	-1.0	P	170010000	*		COLD LEG COLLECTOR	
+		1.0	P	230010000	*		LOWER PLENUM	
-----								
* DIFFERENCE OF DP'S OVER HOT AND COLD LEG								
20500400	DPBCHLG	SUM	1.0	0.0		1		0
20500401	0.0	1.0	CNTRLVAR	3	-1.0	CNTRLVAR	2	
-----								
* VAPOR GENERATION IN CORE								
20500500	VGENCORE	SUM	1.0	0.0		1		0
20500501	0.0	1.0	VAPGEN	100010000	1.0	VAPGEN	100020000	
+		1.0	VAPGEN	100030000	1.0	VAPGEN	100040000	
+		1.0	VAPGEN	100050000	1.0	VAPGEN	100060000	
+		1.0	VAPGEN	100070000	1.0	VAPGEN	100080000	
+		1.0	VAPGEN	100090000	1.0	VAPGEN	100100000	
+		1.0	VAPGEN	100110000				
* VAPOR CONDENSATION IN STEAM GENERATOR PRIMARY SIDE								
20500600	VCOND SG	SUM	1.0	0.0		1		0
20500601	0.0	1.0	VAPGEN	162010000	1.0	VAPGEN	164010000	
+		1.0	VAPGEN	162020000	1.0	VAPGEN	164020000	
+		1.0	VAPGEN	162030000	1.0	VAPGEN	164030000	
+		1.0	VAPGEN	162040000	1.0	VAPGEN	164040000	
+		1.0	VAPGEN	162050000	1.0	VAPGEN	164050000	
+		1.0	VAPGEN	162060000	1.0	VAPGEN	164060000	
* VAPORIZATION ALONG UPPER PLENUM AND HOT LEG								
20500800	VGENH LG	SUM	1.0	0.0		1		0
20500801	0.0	1.0	VAPGEN	105010000	1.0	VAPGEN	105020000	
+		1.0	VAPGEN	105030000	1.0	VAPGEN	105040000	
+		1.0	VAPGEN	110010000	1.0	VAPGEN	125010000	
+		1.0	VAPGEN	120010000	1.0	VAPGEN	120020000	
+		1.0	VAPGEN	120030000	1.0	VAPGEN	120040000	
+		1.0	VAPGEN	140010000	1.0	VAPGEN	140020000	
+		1.0	VAPGEN	140030000	1.0	VAPGEN	140040000	
+		1.0	VAPGEN	150010000				
* STEAM CONDENSATION IN COLD LEG SIDE COLLECTOR & FALLING PIPE								
20500900	VCONDCL	SUM	1.0	0.0		1		0
20500901	0.0	1.0	VAPGEN	170010000	1.0	VAPGEN	180010000	
* EXCESS VAPOR GENERATION								
20500700	VGENEXCS	SUM	1.0	0.0		1		0
20500701	0.0	1.0	CNTRLVAR	5	1.0	CNTRLVAR	6	
+		1.0	CNTRLVAR	8	1.0	CNTRLVAR	9	
-----								

## \* HEAT INPUT IN CORE

20502000 QCORE		SUM	1.0	0.0	1	0
20502001	0.0	Q	100010000	1.0	Q	100020000
+		Q	100030000	1.0	Q	100040000
+		Q	100050000	1.0	Q	100060000
+		Q	100070000	1.0	Q	100080000
+		Q	100090000	1.0	Q	100100000
+		Q	100110000			

## \* HEAT INPUT IN SG SECONDARY SIDE

20502100 QSGSEC		SUM	1.0	0.0	1	0
20502101	0.0	Q	250010000	1.0	Q	250020000
+		Q	250030000			

## \* EXCESS HEAT INPUT

20502200 QLEXCESS		SUM	1.0	0.0	1	0
20502201	0.0	CNTRLVAR 20	-1.0		CNTRLVAR 21	

## \* HEAT LOSSES AT UPPER PLENUM

20502500 QLOSSUP		SUM	1.0	0.0	1	0
20502501	0.0	Q	105010000	1.0	Q	105020000
+		Q	105030000	1.0	Q	105040000
+		Q	115010000	1.0	Q	115020000
+		Q	110010000			

## \* HEAT LOSSES AT HOT LEG

20502600 QLOSSHL		SUM	1.0	0.0	1	0
20502601	0.0	Q	120010000	1.0	Q	120020000
+		Q	120030000	1.0	Q	120040000
+		Q	140010000	1.0	Q	140020000
+		Q	140030000	1.0	Q	140040000
+		Q	125010000			

## \* HEAT LOSSES AT COLD LEG

20502700 QLOSSCL		SUM	1.0	0.0	1	0
20502701	0.0	Q	180010000	1.0	Q	185010000
+		Q	190010000	1.0	Q	195010000

## \* HEAT LOSSES AT DOWNCOMER

20502800 QLOSSDC		SUM	1.0	0.0	1	0
20502801	0.0	Q	220010000	1.0	Q	220020000
+		Q	220030000	1.0	Q	220040000
+		Q	220050000	1.0	Q	220060000
+		Q	210010000			

## \* SUM OF LOSSES

20502400 QLOSSSUM		SUM	1.0	0.0	1	0
20502401	0.0	CNTRLVAR 25	1.0		CNTRLVAR 26	
+		CNTRLVAR 27	1.0		CNTRLVAR 28	

## \* TOTAL EXCESS HEAT INPUT

20502300 QTEXCESS		SUM	1.0	0.0	1	0
20502301	0.0	CNTRLVAR 22	1.0		CNTRLVAR 24	

## \* HYDRODYNAMIC COMPONENTS:

\*

## \* CORE

\*

	CORE	PIPE		
1000000				
1000001	11			
1000101	0.00219	11		
100030.	0.232	11		
1000401	0.0	11		
1000601	90.0	11		
1000801	5.E-5	7.6E-3	11	
1000901	4.81	4.81	10	
1001001	00	11		
1001101	1000	10		

\*

## \* INITIAL VALUES (P, UF, UG, VOIDG)

\*

1001201	0	7.0025E5	4.14E5	2.570E6	0.0	0.0	1
1001202	0	6.9000E5	4.29E5	2.570E6	0.0	0.0	2
1001203	0	6.9590E5	4.52E5	2.570E6	0.0	0.0	3
1001204	0	6.9370E5	4.81E5	2.570E6	0.0	0.0	4
1001205	0	6.9150E5	5.17E5	2.570E6	0.0	0.0	5
1001206	0	6.8940E5	5.54E5	2.570E6	0.0	0.0	6
1001207	0	6.8730E5	5.89E5	2.570E6	0.0	0.0	7
1001208	0	6.8516E5	6.21E5	2.570E6	0.0	0.0	8
1001209	0	6.8304E5	6.45E5	2.570E6	0.0	0.0	9
1001210	0	6.8093E5	6.60E5	2.570E6	0.0	0.0	10
1001211	0	6.7883E5	6.60E5	2.570E6	0.0	0.0	11
1001300	1						
1001301	0.072	0.0	0.0	10			

\*

	CCRTOUPL	SINGLJUN		
1020000				
1020101	100010000	10500000		
1020102	1.08E-3	7.9	7.9	1000
1020201	1	0.072	0.0	0.0

\*

## \* UPPER PLENUM, LOWER PART

\*

	UPPLELOW	PIPE					
1050000							
1050001	4						
1050101	0.00312	4					
1050301	0.572	4					
1050401	0.000	4					
1050601	90.0	4					
1050801	5.0E-5	0.063	4				
1050901	3.22	3.22	3				
1051001	00	4					
1051101	1000	3					
1051201	0	6.751E5	6.59E5	2.570E6	0.0	0.0	1
105120	0	6.700E5	6.59E5	2.570E6	0.0	0.0	2
1051203	0	6.648E5	6.58E5	2.570E6	0.0	0.0	3
1051204	0	6.596E5	6.56E5	2.570E6	0.0	0.0	4
1051300	1						
1051301	0.072	0.0	0.0	3			

\*

## \* UPPER PLENUM ( TO THE HOT LEG )

\*

	UPLCONX	BRANCH							
1100000									
1100001	3	1							
1100101	0.00312	0.858	0.0	0.0	90.0	0.858	5.0E-5	0.063	00
1100200	0	6.5309E5	6.52E5	2.570E6		0.0			
1100101	105010000	110000000	0.00312	3.26	3.26	1000			
1102101	110010000	120000000	0.000412	6.22	6.22	1002			
1103101	110010000	115000000	0.00312	3.25	3.25	1000			
1101201	0.072	0.0	0.0						
1102201	0.072	0.0	0.0						



1103201 0.0 0.0 0.0

\* UPPER PLENU FROM THE HOT LEG )

UPHEAD	PIPE							
1150000	2							
1150101	0.00312	1						
1150102	0.0553	2						
1150301	0.414	1						
1150302	0.1	2						
1150401	0.0	2						
1150601	90.0	2						
1150801	5.E-5	0.063	1					
1150802	5.E-5	0.265	2					
1150901	5.16	5.16	1					
1151001	00	2						
1151101	1100	1						
1151201	0	6.512E5	6.4CE5	2.570E6	0.0	0.0	1	
1151202	4	6.598E5	415.0	8.0E-4	0.0	0.0	2	
1131300	1							
1151301	0.0	0.0	0.0	1				

\* HOT LEG ( FIRST PART )

HTLGDOWN	PIPE							
1200000	4							
1200101	0.00412	4						
1200301	0.5685	4						
1200501	0.0	4						
1200601	-60.0	4						
1200701	-0.4925	4						
1200801	5.0E-5	0.0229	4					
1200901	1.9	1.9	3					
1201001	00		4					
1201101	1000		3					
1201201	0	6.5950E5	6.512E5	2.570E6	0.0	0.0	2	
1201202	0	6.6440E5	6.490E5	2.570E6	0.0	0.0	4	
1201300	1							
1201301	0.072	0.0	0.0	3				

\* HOT LEG ( CONNECTION TO THE PRESSURISER )  
\*\*\*\*\* PRESSURIZER REMOVED BY JT

HTLGFLAT	BRANCH								
1250000	2	1							
1250101	0.412E-3	0.559	0.0	0.0	0.0	0.0	5.0E-5	0.0229	00
1250200	0	6.707E5	6.48E5	2.570E6	0.0				
1251101	120010000	125000000	4.12E-4	3.26	3.26	1000			
1252101	125010000	140000000	4.12E-4	3.26	3.26	1000			
1251201	0.072	0.0	0.0						
1252201	0.072	0.0	0.0						

\* HOT LEG ( TO THE STEAM GENERATOR )

HOTLEGUP	PIPE		
1400000	4		
1400101	4.12E-4	4	
1400301	0.580	4	
1400501	0.0	4	
1400601	90.0	4	
1400701	0.580	4	

```

1400801 5.0E-5 0.0229 4
1400901 3.22 3.22 3
1401001 00 4
1401101 1000 3
* INITIAL CONDITIONS
1401201 0 6.759E5 6.460E5 2.570E6 0.0 0.0 2
1401202 0 6.650E5 6.442E5 2.570E6 0.0 0.0 4
1401300 1
1401301 0.072 0.0 0.0 3

```

```

*-----*
*
* STEAM GENERATOR, EXTENDED VERSION 2/JH 1.9.87

```

```

*
* HOT LEG SIDE COLLECTOR (2 BRANCHES WITH CROSSFLOW JUNCTIONS TO SG TUBES)

```

```

1500000 HOTCOLLW BRANCH
1500001 3 1 * NO CF JUNS, INIT=FLOW
* GEOMETRY
1500101 2.043E-3 0.200 0.0 0.0 90.0 0.200
+ 5.0E-5 0.051 00
* VOLUME INITIAL CONDITIONS: PRESS, UF, UG, VOIDG
1500200 0 6.485E5 6.430E5 2.570E6 0.0
* CONNECTIONS
1501101 140010000 150000000 4.12E-4 5.5 6.1 1000
1502101 150000000 162000000 7.96E-4 8.7 4.1 1002
1503101 150010000 154000000 2.043E-3 7.9 5.3 1000
* JUNCTION INITIAL CONDITIONS: MFLOWL, MFLOWG, INTERPHASE
1501201 0.072 0.0 0.0
1502201 0.030 0.0 0.0
1503201 0.042 0.0 0.0

```

```

1540000 HOTCOLUP BRANCH
1540001 1 1 * NO CF JUNS, INIT=FLOW
* GEOMETRY
1540101 2.043E-3 0.120 0.0 0.0 90.0 0.120
+ 5.0E-5 0.051 00
* VOLUME INITIAL CONDITIONS: PRESS, UF, UG, VOIDG
1540200 0 6.470E5 6.430E5 2.570E6 0.0
* CONNECTIONS
1541101 154000000 162000000 7.96E-4 17.9 13.0 1002
* JUNCTION INITIAL CONDITIONS: MFLOWL, MFLOWG, INTERPHASE
1541201 0.042 0.0 0.0

```

```

*
* STEAM GENERATOR, PRIMARY SIDE TUBING (2 PIPES)

```

```

1620000 SGPRIBOT PIPE
1620001 6 * NO OF PIPE VOLUMES
1620101 0.7964E-3 6 * AREAS
1620301 0.762 2 * LENGTHS
1620302 2.313 4
1620303 0.762 6
1620501 90.0 3 * HORIZ ANGLES (U-TUBE)
1620503 -90.0 6
1620601 0.0 6 * VERTIC ANGLES
1620701 0.0 6 * ELEV CHANGES
1620801 5.0E-5 0.013 6 * FRICTION DATA
1620901 0.7 0.7 2 * JUNCTION LOSS COEFF
1620902 2.11 2.11 3
1620903 0.7 0.7 5
1621001 00 6 * VOL FLAGS: FRIC+NONEQ
1621101 1000 5 * JUN FLAGS: NOCHOK, SMOOTH, 2VEL, CENTRAL
* INITIAL VOLUME CONDITIONS: PRESS, UF, UG, VOIDG
1621201 0 6.485E5 5.01E5 2.570E6 0.0 0.0 1
1621202 0 6.485E5 4.67E5 2.570E6 0.0 0.0 2
1621203 0 6.485E5 4.38E5 2.570E6 0.0 0.0 3

```

```

1621204    0  6.485E5  4.28E5    2.570E6  0.0    0.0    4
1621205    0  6.485E5  4.26E5    2.570E6  0.0    0.0    5
1621206    0  6.485E5  4.25E5    2.570E6  0.0    0.0    6
* INITIAL JUNCTION CONDITIONS
1621300    1                                * FLOWS FOLLOW
1621301    0.030    0.0    0.0    5
*
1640000    SGPRITOP    PIPE
1640001    6                                * NO OF PIPE VOLUMES
1640101    0.7964E-3    6    * AREAS
1640301    0.762    2    * LENGTHS
1640302    2.313    4
1640303    0.762    6
1640501    90.0    3    * HORIZ ANGLES
1640503    -90.0    6
1640601    0.0    6    * VERTIC ANGLES
1640701    0.0    6    * ELEV CHANGES
1640801    5.0E-5    0.013    6    * FRICTION DATA
1640901    0.7    0.7    2    * JUNCTION LOSS COEFF
1640902    2.11    2.11    3
1640903    0.7    0.7    5
1641001    00    6    * VOL FLAGS: FRIC+NONEQ
1641101    1000    5    * JUN FLAGS: NOCHOK, SMOOTH, 2VEL, FULL I
* INITIAL VOLUME CONDITIONS: PRESS, UF, UG, VOIDG
1641201    0  6.470E5  5.47E5    2.570E6  0.0    0.0    1
1641202    0  6.470E5  4.96E5    2.570E6  0.0    0.0    2
1641203    0  6.470E5  4.48E5    2.570E6  0.0    0.0    3
1641204    0  6.470E5  4.32E5    2.570E6  0.0    0.0    4
1641205    0  6.470E5  4.29E5    2.570E6  0.0    0.0    5
1641206    0  6.470E5  4.26E5    2.570E6  0.0    0.0    6
* INITIAL JUNCTION CONDITIONS
1641300    1                                * FLOWS FOLLOW
1641301    0.042    0.0    0.0    5
*
* COLD LEG SIDE COLLECTOR
*
1700000    COLDCOLL    BRANCH
1700001    3    1    * NO OF JUNS, INIT=FLOWS
* GEOMETRY
1700101    2.043E-3    0.200    0.0    0.0    -90.0    -0.200
+    5.0E-5    0.0E+00
* VOLUME INITIAL CONDITIONS: PRESS, UF, UG, VOIDG
1700200    0  6.485E5  4.266E5    2.570E6  0.0
* CONNECTIONS
1701101    170010000    180000000    4.12E-4    6.1    4.5    1000
1702101    162010000    170000000    7.96E-4    4.1    8.7    1001
1703101    174010000    170000000    2.043E-3    7.1    7.9    1000
* JUNCTION INITIAL CONDITIONS: MFLOWL, MFLOWG, INTERPHASE
1701201    0.072    0.0    0.0
1702201    0.030    0.0    0.0
1703201    0.042    0.0    0.0
*
1740000    COLDCOLU    BRANCH
1740001    1    1    * NO OF JUNS, INIT=FLOWS
* GEOMETRY
1740101    2.043E-3    0.120    0.0    0.0    -90.0    -0.120
+    5.0E-5    0.051    00
* VOLUME INITIAL CONDITIONS: PRESS, UF, UG, VOIDG
1740200    0  6.470E5  4.245E5    2.570E6  0.0
* CONNECTIONS
1741101    164010000    174000000    7.96E-4    11.0    13.9    1001
* JUNCTION INITIAL CONDITIONS: MFLOWL, MFLOWG, INTERPHASE
1741201    0.042    0.0    0.0
*
-----
* COLD LEG

```

```

*
1800000      CLGUP  SNGLVOL
* GEOMETRY
1800101      4.12E-4  2.32  0.0  0.0  -90.0  -2.32
+           5.0E-5  0.0229  00
* INITIAL COND
1800200      0  6.601E5  4.24E5  2.570E6  0.0
*
1830000      COLDLEG1  SNGLJUN
1830101      180010000  185000000
1830102      0.0  9.6  9.6  1000
1830201      1  0.072  0.0  0.0
*
1850000      CLGRISE  SNGLVOL
1850101      4.12E-4  2.30  0.0  0.0  60.0
1850102      2.0  5.00E-5  0.0  00
1850200      0  6.614E5  4.23E5  2.570E6  0.0
*
1870000      COLDLEG2  SNGLJUN
1870101      185010000  190000000
1870102      0.0  9.6  9.6  1000
1870201      1  0.072  0.0  0.0
*
1900000      CLGDOWN  SNGLVOL
1900101      4.12E-4  1.41  0.0  0.0  -90.0
1900102      -1.41  5.0E-5  0.0  00
1900200      0  6.565E5  4.21E5  2.570E6  0.0
*
1930000      COLDLEG3  SNGLJUN
1930101      190010000  195000000
1930102      0.0  9.6  9.6  1000
1930201      1  0.072  0.0  0.0
*
1950000      CLGFLAT  SNGLVOL
1950101      4.12E-4  3.40  0.0  0.0  0.0
1950102      0.0  5.0E-5  0.0  00
1950200      0  6.650E5  4.19E5  2.570E6  0.0
*
-----
* DOWNCOMER ( UPPER PART )
*
*2050000      DCMRHEAD  SNGLVOL
*2050101      8.04E-4  0.61  0.0  0.0  90.0
*2050102      0.61  5.0E-5  0.0  00
*2050200      0  4.336E5  4.20E5  2.570E6  0.0
*
* DOWNCOMER ( CONNECTION TO THE COLD LEG )
*
2100000      DCMRCONX  BRANCH
2100001      2  1
2100101      8.04E-4  1.22  0.0  0.0  -90.0
2100102      -1.22  5.0E-5  0.0  00
2100200      0  6.649E5  4.18E5  2.570E6  0.0
2101101      195010000  210000000  0.0  11.82  11.82  1001
2102101      210010000  220000000  0.0  9.94  9.94  1000
*2103101      210000000  205000000  0.0  0.2  0.2  1000
2101201      0.072  0.0  0.0
2102201      0.072  0.0  0.0
*
* DOWNCOMER
*
2200000      DOWNCOMR  PIPE
2200001      6
2200101      0.804E-3  4
2200105      1.225E-3  6
2200301      1.0945  1

```

2200302	1.22275	3						
2200305	1.283	6						
2200601	-90.0	6						
2200801	5.0E-5	0.032	4					
2200802	5.0E-5	0.0305	6					
2200901	1.1	1.1	5					
2201001	00	6						
2201104	1000	5						
2201201	0	6.758E5	4.177E5	2.570E6	0.0	0.0	1	
2201202	0	6.866E5	4.167E5	2.570E6	0.0	0.0	2	
2201203	0	6.981E5	4.157E5	2.570E6	0.0	0.0	3	
2201204	0	7.098E5	4.146E5	2.570E6	0.0	0.0	4	
2201205	0	7.219E5	4.136E5	2.570E6	0.0	0.0	5	
2201206	0	7.340E5	4.125E5	2.570E6	0.0	0.0	6	
2201300	1							
2201301	0.072	0.0	0.0	5				

\* -----  
\* LOWER PLENUM

\* NEW LOWER PLENUM

2300000	LPFLAT2	BRANCH						
2300001	2	1						
2300101	1.83E-3	0.740	0.0	0.0	0.0	0.0	5.0E-5	0.0 00
2300200	0	7.40E5	4.126E5	2.57E6	0.0			
2301101	220010000	230000000	0.0	14.89	14.89	1000		
2302101	230010000	240000000	0.0	14.29	14.29	1000		
2301201	0.072	0.0	0.0					
2302201	0.072	0.0	0.0					

\* LOWPLUP PIPE

2400000	4							
2400101	4.083E-3	2						
2400102	2.736E-3	4						
2400301	1.20	1						
2400302	1.20	2						
2400303	0.884	3						
2400304	0.826	4						
2400601	90.0	4						
2400801	5.0E-5	0.0						
2400901	18.63	18.63	1					* JUNCTION LOSS COEFF.
2400902	27.63	27.63	3					
2401001	00	4						
2401101	1000	3						
2401201	0	7.343E5	4.129E5	2.570E6	0.0	0.0	1	
2401202	0	7.231E5	4.134E5	2.570E6	0.0	0.0	2	
2401203	0	7.133E5	4.137E5	2.570E6	0.0	0.0	3	
2401204	0	7.052E5	4.139E5	2.570E6	0.0	0.0	4	
2401300	1							
2401301	0.072	0.0	0.0	3				

2450000	LPTOCORE	SNGLJUN						
2450101	240010000	100000000						
2450102	0.0	16.87	16.87	1000				
2450201	1	0.072	0.0	0.0				

\* -----  
\* STEAM GENERATOR SECONDARY SIDE  
\* (PIPE OF 3 COMPONENTS, SNGLJUN, TMPDVOL)

2500000	SGSEC	PIPE						
2500001	3							* NO OF VOLS
2500101	0.7501	2						* FLOW AREAS
2500102	0.8302	3						
2500301	0.120	2						* HEIGHTS



2500302 0.166 3  
 2500601 90.0 3 \* VERTICAL ANGLES  
 2500301 5.0E-5 0.0 3 \* ROUGHNESS, DRY  
 2500901 1.3 1.3 2 \* JUNCTION LOSSES  
 2501001 00 3 \* VOL FLAGS: FRICT, NON-EQUIL  
 2501101 1000 2 \* JUN FLAGS: NOCHOK, SMOOTH, 2VEL, IN  
 2501201 2 1.035E5 1.5E-5 0.0  
 + 0.0 0.0 2 \* INITIAL VOL COND: PRESS, STAT X  
 2501202 1 1.023E5 6.3E-4 0.0 0.0 0.0 3  
 2501300 0 \* INITIAL JUN COND:  
 2501301 0.0 0.0 0.0 2 \* VELOCITIES

2560000 SECTOERY SNGLJUN  
 2560101 250010000 260000000 0.05 10.0 5.0 1100  
 2560201 0 0.00 0.00 0.0

2600000 SECBRY TMDPVOL  
 \* SECONDARY SIDE BOUNDARY CONDITIONS  
 2600101 1.0 0.20 0.0 0.0 0.0 0.0 5.0E-5 0.0 10  
 \* BOUNDARY COND: PRESSURE = 1.02 BAR, QUALITY 0.07 % (=> VOIDG=0.52)  
 2600200 2  
 2600201 0.0 1.02E5 0.0007

-----

\* LEAK JUNCTION - TRY CLOSING

3000000 LEAK TMDPJUN \* SNGLJUN  
 3000101 230000000 310000000 9.2E-4 \* 10.0 1.0 1000  
 \* 3000201 0 0.0 0.0 0.0  
 3000200 0  
 3000201 0.0 0.0 0.0 0.0

\* LEAK BOUNDARY

3100000 LEAKBDY TMDPVOL  
 3100101 1.0E-3 0.5 0.0 0.0 0.0 0.0 5.0E-5 0.0 00  
 3100200 0 0 UF 220060000  
 \* PRESSURE & INTERNAL ENERGIES & VOIDG FOLLOW UF 220-06  
 3100201 4.00E5 7.4E5 4.00E5 2.573E6 0.0  
 3100202 4.30E5 7.4E5 4.30E5 2.573E6 0.0

-----

\* HEAT STRUCTURES

\* STEAM GENERATOR TUBES (2 SIMILAR STRUCTURES  
 WITH DIFFERENT BOUNDARY VOLUMES)

\* LOWER PART

\* NO OF STRS, NO OF MESHP, CYL, STDY-ST-INIT, LEFT BDRY COORD  
 11621000 6 3 2 1 6.5E-3  
 11621100 0 1 \* MESH LOC FLAG, MESH FORMAT FLAG  
 11621101 2 7.5E-3 \* NO OF INTERVALS, RIGHT BDRY COORD  
 11621201 3 2 \* COMPOSITION NO, INTERVAL NO  
 11621301 0.0 2 \* SOURCE TERM, "-"  
 11621400 0 \* INITIAL COND FLAG: TEMPERATURES FOLLOW  
 11621401 375.0 1 \* MESH POINT TEMPERATURES  
 11621402 374.0 2  
 11621403 374.0 3  
 \* LEFT HYDROD BDRY VOLUME, INCR, BDRY=CONV, SURF AREA FLG, -VAL, STR NO  
 11621501 162000000 10000 1 1 4.5720 2  
 11621502 162030000 10000 1 1 13.878 4  
 11621503 162050000 10000 1 1 4.5720 6  
 \* RIGHT (AS LEFT)  
 11621601 250010000 0 1 1 4.5720 2



```

11621602 250010900      0      1      1      13.878  4
11621603 250010000      0      1      1      4.5720  6
11621701 0      0.0      0.0      0.0      6      * NO INTERNAL SOURCE
* LEFT BDRY DATA: CHF FLAG, DRY, HEATED EQU. DIAM, LENGTH
11621801 0      0.013  0.013  0.762  2
11621802 0      0.013  0.013  2.313  4
11621803 0      0.013  0.013  0.762  6
* RIGHT AS LEFT
11621901 0      0.015  0.015  0.762  2
11621902 0      0.015  0.015  2.313  4
11621903 0      0.015  0.015  0.762  6

```

```

* UPPER PART
11641000 6 3 2 1 6.5E-3
11641100 0 1
11641101 2 7.5E-3
11641201 3 2
11641301 0.0 2
11641400 0
11641401 375.0 1
11641402 374.0 2
11641403 374.0 3
11641501 164010000      10000  1  1  4.5720  2
11641502 164030000      10000  1  1  13.878  4
11641503 164050000      10000  1  1  4.5720  6
11641601 250020000      0      1  1  4.5720  2
11641602 250020000      0      1  1  13.878  4
11641603 250020000      0      1  1  4.5720  6
11641701 0      0.0      0.0      0.0      6
11641801 0      0.013  0.013  0.762  2
11641802 0      0.013  0.013  2.313  4
11641803 0      0.013  0.013  0.762  6
11641901 0      0.015  0.015  0.762  2
11641902 0      0.015  0.015  2.313  4
11641903 0      0.015  0.015  0.762  6

```

```

* FUEL RODS:
* CORE (MgO) + CLADDING (S-STEEL)

```

```

*
* NSTR NP CYL STDY=YES LEFT COORD
11003000 11 5 2 1 0.0
11003100 0 1 * MESH LOC = ENTER HERE
11003101 3 3.55E-3 * NO OF INTERVALS, RIGHT COORDINATE
11003102 1 4.55E-3
11003201 2 3 * COMPOSITION 2 (MGO) / FIRST 3 INTERVALS
11003203 1 4 * COMPOSITION 1 (STEEL) / 4TH INTERVAL
11003301 0.0 1 * SOURCE = 1.0 IN MID-MGO, 0.0 ELSEWHERE
11003302 1.0 2
11003303 0.0 4
11003400 -1 * INIT. TEMP FLAG = ALL STRS SEPARATELY

```

```

* MESH POINT TEMPS FOR ALL HEAT STRUCTURES
11003401 372.27 372.27 372.27 372.27 372.27
11003402 383.26 383.26 382.34 381.02 380.70
11003403 397.29 397.29 395.25 392.32 391.64
11003404 409.18 409.18 406.32 402.23 401.30
11003405 422.07 422.07 418.37 413.07 411.88
11003406 429.58 429.58 425.67 420.08 418.85
11003407 434.09 434.09 430.32 424.93 423.76
11003408 434.34 434.34 431.16 426.61 425.63
11003409 430.29 430.29 428.11 424.97 424.29
11003410 422.87 422.87 421.91 420.51 420.21
11003411 415.07 415.07 415.07 415.07 415.07
11003501 0 0 0 1 0.0 11 * LEFT BDRY DATA
11003601 100010000 10000 1 1 4.408 11 * RIGHT "-"

```

ID	Vol	Temp	Rad	Surf	Surf	Surf	Notes
11003701	100	0.0	0.0	0.0	1		* SOURCE DISTRIBUTION
11003702	100	0.0407	0.0	0.0	2		
11003703	100	0.0887	0.0	0.0	3		
11003704	100	0.1221	0.0	0.0	4		
11003705	100	0.1559	0.0	0.0	5		
11003706	100	0.1628	0.0	0.0	6		
11003707	100	0.1559	0.0	0.0	7		
11003708	100	0.1313	0.0	0.0	8		
11003709	100	0.0908	0.0	0.0	9		
11003710	100	0.0406	0.0	0.0	10		
11003711	100	0.0	0.0	0.0	11		
11003801	0	0.0	0.0	0.232	11		* LEFT EXTRA DATA
11003901	0	7.6E-3	3.1E-3	0.232	11		* RIGHT -"-

\* CORE HOUSING (EXTERNAL HEATERS)

ID	NSTR	NP	RECT	STDY=YES	LEFT COORD	Notes
11005000	9	3	1	1	0.0	
11005100	0	1				* MESH LOC = ENTER HERE
11005101	2	5.0E-3				* NO OF INTERVALS, RIGHT COORDINATE
11005203	1	2				* COMPOSITION 1 (STEEL)
11005301	0.0	2				* NO (RADIAL) SOURCE
11005400	-1					* INIT. TEMP FLAG: SEPARATE FOR ALL STRS
11005401	389.32		391.02		392.72	
11005402	393.14		394.83		396.52	
11005403	398.02		399.70		401.39	
11005404	404.00		405.68		407.35	
11005405	410.23		411.90		413.57	
11005406	416.24		417.90		419.57	
11005407	421.44		423.10		424.76	
11005408	425.34		426.99		428.65	
11005409	427.61		429.27		430.92	
LEFT BDY DATA						
11005501	100020000	10000	1	0	0.03762	9
RIGHT BDY DATA (VOL 310010000 IS USED AS A DUMMY VOLUME)						
WITH FIXED HEAT FLUX FROM TABLE 101						
11005601	310010000	0	2101	0	0.03762	9
NO (AXIAL) SOURCE						
11005701	0	0.0	0.0	0.0	0.0	9
LEFT EXTRA DATA						
11005801	0	7.6E-3	0.0	0.0	0.232	9

-----  
UPPER PLENUM (ENVIRONMENTAL LOSSES)

ID	NSTR	NMP	CYL	STDY=Y	LEFT COORD	Notes
1101000	7	5	2	1	0.0315	
1101100	0	1				* MESH LOC & FORMAT
1101101	2	0.034				* INTERVALS, RIGHT COORD
1101102	2	0.100				
1101201	1	2				* COMPOSITION, INTERVALS
1101202	4	4				
1101301	0.0	4				* RADIAL SOURCE DISTRIB
1101401	413.3	1				* INITIAL TEMPERATURES
1101403	413.2	3				
1101404	340.7	4				
1101405	297.2	5				
LEFT BOUNDARY DATA						
1101501	105010000	10000	1	1	0.572	4
1101502	110010000	0	1	1	0.858	5
1101503	115010000	10000	1	1	0.414	7
RIGHT BOUNDARY						
1101601	-200	0	3110	1	0.572	4
1101602	-200	0	3110	1	0.858	5
1101603	-200	0	3110	1	0.414	7

\* AXIAL SOURCE  
 11101701 0 0.0 0.0 0.0 7  
 \* ADDITIONAL LEFT BOUNDARY DATA  
 11101801 0 0.063 0.063 0.0 7

\* HOT LEG (ENVIRONMENTAL LOSSES)

\*  
 \* NSTR NMP CYL STDY=Y LEFT COORD  
 11201000 9 5 2 1 0.01145  
 11201100 0 1 \* MESH LOC & FORMAT  
 11201101 2 0.01345 \* INTERVALS, RIGHT COORD  
 11201102 2 0.0635  
 11201201 1 2 \* COMPOSITION, INTERVALS  
 11201202 4 4  
 11201301 0.0 4 \* RADIAL SOURCE DISTRIB  
 11201401 413.1 3 \* INITIAL TEMPERATURES  
 11201402 336.6 4  
 11201403 297.7 5  
 \* LEFT BOUNDARY DATA  
 1201501 120010000 10000 1 1 0.5685 4  
 1201502 125010000 0 1 1 0.559 5  
 1201503 140010000 10000 1 1 0.580 9  
 \* RIGHT BOUNDARY  
 1201601 -200 0 3110 1 0.5685 4  
 1201602 -200 0 3110 1 0.559 5  
 1201603 -200 0 3110 1 0.580 9  
 AXIAL SOURCE  
 1201701 0 0.0 0.0 0.0 9  
 ADDITIONAL LEFT BOUNDARY DATA  
 1201801 0 0.0229 0.0229 0.0 9

COLD LEG (ENVIRONMENTAL LOSSES)

NSTR NMP CYL STDY=Y LEFT COORD REFLOOD=NO  
 1901000 4 5 2 1 0.01145 0  
 1901100 1201 \* MESH DATA EQUAL TO HOT LEG  
 1901401 374.4 3  
 1901402 322.3 4  
 1901403 296.2 5  
 LEFT BOUNDARY DATA  
 1901501 180010000 0 1 1 2.320 1  
 1901502 185010000 0 1 1 2.300 2  
 1901503 190010000 0 1 1 1.410 3  
 1901504 195010000 0 1 1 3.400 4  
 RIGHT BOUNDARY  
 1901601 -200 0 3120 1 2.320 1  
 1901602 -200 0 3120 1 2.300 2  
 1901603 -200 0 3120 1 1.410 3  
 1901604 -200 0 3120 1 3.400 4  
 AXIAL SOURCE  
 1901701 0 0.0 0.0 0.0 4  
 ADDITIONAL LEFT BOUNDARY DATA  
 1901801 0 0.063 0.063 0.0 4

DOWNCOMER

NSTR NMP CYL STDY=Y LEFT COORD  
 201000 7 5 2 1 0.019  
 201100 0 1 \* MESH LOC & FORMAT  
 201101 2 0.021 \* INTERVALS, RIGHT COORD  
 201102 2 0.071  
 201201 1 2 \* COMPOSITION, INTERVALS  
 201202 4 4  
 201301 0.0 4 \* RADIAL SOURCE DISTRIB  
 201401 372.1 3 \* INITIAL TEMPERATURES  
 201402 324.0 4

12201403 296.5 5  
 \* LEFT BOUNDARY DATA  
 12201501 210010000 0 1 1 1.220 1  
 12201502 220010000 0 1 1 0.880 2  
 12201503 220020000 10000 1 1 1.22275 4  
 12201504 220040000 10000 1 1 1.2830 7  
 \* RIGHT BOUNDARY  
 12201601 -200 0 3120 1 1.220 1  
 12201602 -200 0 3120 1 0.880 2  
 12201603 -200 0 3120 1 1.22275 4  
 12201604 -200 0 3120 1 1.2830 7  
 \* AXIAL SOURCE  
 12201701 0 0.0 0.0 0.0 7  
 \* ADDITIONAL LEFT BOUNDARY DATA  
 12201801 0 0.0380 0.0380 0.0 7

\*\*\*\*\*

\* COMPOSITION TABLES

-----  
 \* MATERIAL PROPERTIES FOR COMPOSITION 1, CLADDING & CORE SHROUD

0100100 TBL/FCTN 1 1  
 THERMAL CONDUCTIVITY  
 0100101 293.15 14.2  
 0100102 323.15 15.5  
 0100103 373.15 16.0  
 0100104 573.15 18.3  
 0100105 723.15 21.0  
 0100106 973.15 24.1  
 0100107 1173.15 27.6  
 VOLUMETRIC HEAT CAPACITY  
 0100151 293.15 3.718E6  
 0100152 323.15 3.763E6  
 0100153 373.15 4.069E6  
 0100154 573.15 4.408E6  
 0100155 773.15 4.748E6  
 0100156 1273.15 5.027E6

-----  
 MATERIAL PROPERTIES OF MGO, COMPOSITION 2

0100200 TBL/FCTN 1 1  
 THERMAL CONDUCTIVITY  
 0100201 273.15 7.10  
 0100202 473.15 5.48  
 0100203 673.15 3.85  
 0100204 723.15 3.46  
 0100205 773.15 3.18  
 0100206 823.15 2.98  
 0100207 873.15 2.82  
 0100208 923.15 2.68  
 0100209 973.15 2.57

VOLUMETRIC HEAT CAPACITY

0100251 273.15 3.300E6  
 0100252 293.15 3.300E6  
 0100253 573.15 3.296E6  
 0100254 673.15 3.323E6  
 0100255 723.15 3.314E6  
 0100256 923.15 3.865E6  
 0100257 973.15 3.884E6

-----  
 PROPERTIES OF COMPOSITION 3, STEAM GENERATOR TUBES, COPPER

\* TYPE COND = TABLE VOLUM. CP = TABLE  
 20100300 TBL/FCTN 1 1

\* THERMAL CONDUCTIVITY (ASSUMED CONSTANT)  
 20100301 385.0

\* VOLUMETRIC HEAT CAPACITY (ASSUMED CONSTANT)  
 20100351 3.435E6

\* -----  
 \* COMPOSITION 4, MINERAL WOOL, LEG OUTER INSULATOR

20100400 TBL/FCTN 1 1  
 \* CONDUCTIVITY  
 20100401 0.16  
 \* VOLUMETRIC HEAT CAPACITY  
 20100451 2.1E5

\* -----  
 \* GENERAL TABLES: POWERS & LOSS BOUNDARY HEAT TRANSFER COEFFICIENTS

\* - FUEL RODS  
 20210000 POWER  
 20210002 0.0 14.0E3  
 20210004 1.0E4 14.0E3

\* - EXTERNAL HEATERS, 5 KW = 13.8 KW/M2  
 20210100 HTRNRATE  
 20210102 0.0 -13.8E3  
 20210104 1.0E4 -13.8E3

\* UPPER PLENUM & HOT LEG  
 20211000 HTC-T  
 20211001 0.0 6.1  
 20211002 10.0 26.1  
 20211003 1.0E4 26.1

\* COLD LEG & DOWNCOMER  
 20212000 HTC-T  
 20212001 0.0 6.1  
 20212001 10.0 26.1  
 20212002 1.0E4 26.1

\* ENVIRONMENT TEMPERATURE  
 20220000 TEMP  
 20220001 0.0 293.0  
 20220002 1.0E4 293.0

\* ----- END OF INPUT -----

APPENDIX D

LISTING OF INPUT DATA FOR TWO-PHASE CASE



= REWET-III NATURAL CIRCULATION, SG 6 INIT /7/ L16-5 / JUHANI HYVARINEN  
 \* ---- MOD2 VERSIGN ----  
 \*  
 \* FILLING RATIO 100 % AND POWER 12+5 kW = THE APPROXIMATE INITIAL STATE  
 \* OF THE LEAK. PRESSURE ABOUT 3.0 BAR  
 \*

\*\*\*\*\*  
 \*  
 100 NEW STDY-ST  
 101 RUN  
 102 SI SI  
 \*

\* CPU-REMAINING CARD  
 \*  
 105 5.0 10.0  
 \*

\* HYDRODYNAMIC SYSTEM CARDS  
 \*

	REF. VOLUME	REF. ELEVATION	FLUID	SYSTEM NAME
120	230010000	0.0	WATER	PRIMARY
121	250010000	9.5	WATER	SECONDRY

\*\*\*\*\*  
 \* TIME STEP CONTROL CARD(S)  
 \*

\* OPTION ssd03: ss= 7 = 4+2+1 = OMIT  
 \* -SECOND BLOCKS OF VOL&JUN DATA  
 \* -HEAT STRUCTURE TEMPERATURES  
 \* d = 2 = OBTAIN MINOR EDITS AT EVERY HYDRODYNAMIC  
 \* TIME STEP  
 \*

*201	10.0	0.5E-6	0.8	00003	1	100	3000
*203	600.0	0.5E-6	0.6666666666	00003	3	450	3000
*202	99.0	0.5E-6	0.2	00003	5	1200	3000
203	180.0	0.5E-6	0.2	00003	5	1500	3000

\*\*\*\*\*  
 \* TRIPS  
 \*

-----  
 \* TRIP FROM SG INLET PRESSURE >= 2.0 MPA (20 BAR) OR <= 0.20 MPA  
 \*

	VARIABLE	OF VOLUME	RELATION	2ND VAR	OF 2ND VOL	+CONST	NOT LATCHED
501	P	140030000	GE	NULL	0	2.00E6	N
502	P	140030000	LE	NULL	0	0.20E6	N

\* TRIP TO STOP NEAR THE STEADY STATE  
 \*

503	MFLOWJ	300000000	LT	NULL	0	1.0E-4	N
504	TIME	0	GT	NULL	0	150.0	L

-----  
 \* LOGICAL TRIP(S)  
 \*

601	501	OR	502	N
602	503	AND	504	N

-----  
 \* TRANSIENT TERMINATING TRIP(S)  
 \*

600 601  
 \*  
 \*\*\*\*\*

\*  
\* MINOR EDIT REQUESTS:

\*  
\* TEMPERATURES

\*  
301 TEMPF 100010000  
302 TEMPF 100110000  
303 TEMPF 125010000  
304 TEMPF 150010000  
305 TEMPF 162010000  
306 TEMPF 162020000  
307 TEMPF 162040000  
308 TEMPF 162050000  
307 TEMPF 162060000  
308 TEMPF 164010000  
309 TEMPF 164020000  
310 TEMPF 164040000  
311 TEMPF 164050000  
312 TEMPF 164060000  
313 TEMPF 170010000  
314 TEMPF 210010000  
315 TEMPF 250010000  
316 TEMPF 250020000  
317 TEMPF 250030000

\*  
\* HEAT INPUTS IN CORE

\*  
320 Q 100010000  
321 Q 100020000  
322 Q 100030000  
323 Q 100040000  
324 Q 100050000  
325 Q 100060000  
326 Q 100070000  
327 Q 100080000  
328 Q 100090000  
329 Q 100100000  
330 Q 100110000

\*  
\* MASS FLOWS

\*  
332 MFLOWJ 102000000  
333 MFLOWJ 162020000  
334 MFLOWJ 164020000  
335 MFLOWJ 220040000  
336 MFLOWJ 300000000

\*  
\* VELOCITIES

\*  
\*349 VELFJ 256000000  
\*350 VELGJ 256000000

\*  
\* PRESSURES

\*  
337 P 140030000  
338 P 100110000  
339 P 250030000

\*  
\* SOME HEAT STRUCTURE TEMPERATURES AT SG TUBES

\*  
\*354 HTTEMP 162100103  
\*355 HTTEMP 162100603  
\*356 HTTEMP 164100103  
\*357 HTTEMP 164100603

\*  
\* HEAT INPUT RATES AT SG TUBES

\*  
 340 Q 162010000  
 341 Q 162020000  
 342 Q 162030000  
 343 Q 162040000  
 344 Q 162050000  
 345 Q 162060000

\*  
 346 Q 164010000  
 347 Q 164020000  
 348 Q 164030000  
 349 Q 164040000  
 350 Q 164050000  
 351 Q 164060000

\* STEAM VOID FRACTIONS

\*  
 353 VOIDG 250010000  
 354 VOIDG 250020000  
 355 VOIDG 250030000

\*  
 356 VOIDG 115010000  
 357 VOIDG 115020000

\*  
 358 QUALA 115020000

\*  
 359 VOIDG 120010000  
 360 VOIDG 120020000  
 361 VOIDG 120030000  
 362 VOIDG 120040000

\*  
 363 VOIDG 105010000  
 364 VOIDG 105020000  
 365 VOIDG 105030000  
 366 VOIDG 105040000

\* CONTROL VARIABLES (DPS, EXCESS STEAM GENERATION, HEAT INPUTS)

\*  
 385 CNTRLVAR 1  
 386 CNTRLVAR 2  
 387 CNTRLVAR 3  
 388 CNTRLVAR 4  
 389 CNTRLVAR 7  
 390 CNTRLVAR 20  
 391 CNTRLVAR 21  
 392 CNTRLVAR 22  
 393 CNTRLVAR 23  
 394 CNTRLVAR 24  
 395 CNTRLVAR 25  
 396 CNTRLVAR 26  
 397 CNTRLVAR 27  
 398 CNTRLVAR 28

\* SPECIALITIES

\*  
 399 CPUTIME 0

\*-----  
 \* CONTROL VARIABLES

\*-----  
 \* PRESSURE DIFFERENCES:  
 \*  $DP = A0 + A1*VAR1 + A2*VAR2$ , DIMENSIONS NOT SCALED (SCALE=1.0)  
 \*  
 \* - OVER CORE

```

*
*      NAME      TYPE  SCALE  INIT.VAL  INIT.FLG=COMPUTE  NO LIMITS
20500100  DPCORE  SUM    1.0    0.0            1            0
*      A0      A1    VAR1 CODE  VOL1 CODE
*      +      A2    VAR2    VOL2
20500101  0.0    1.0    P        100010000      * CORE BOTTOM
*      -1.0   P        100110000      * CORE TOP
*
* - OVER HOT LEG
*
*      NAME      TYPE  SCALE  INIT.VAL  INIT.FLG=COMPUTE  NO LIMITS
20500200  DPHTLEG  SUM    1.0    0.0            1            0
*      A0      A1    VAR1 CODE  VOL1 CODE  +      A2,VAR2,VOL2
20500201  0.0    -1.0   P        150010000      * HOT LEG COLLECTOR
*      1.0    P        230010000      * LOWER PLENUM
*
* - OVER COLD LEG
*
*      NAME      TYPE  SCALE  INIT.VAL  INIT.FLG=COMPUTE  NO LIMITS
20500300  DPCDLEG  SUM    1.0    0.0            1            0
*      A0      A1    VAR1 CODE  VOL1 CODE  +      A2,VAR2,VOL2
20500301  0.0    -1.0   P        170010000      * COLD LEG COLLECTOR
*      1.0    P        230010000      * LOWER PLENUM
*
*-----*
* DIFFERENCE OF DP'S OVER HOT AND COLD LEG
*
20500400  DPBCHLG  SUM    1.0    0.0            1            0
20500401  0.0    1.0    CNTRLVAR  3    -1.0    CNTRLVAR  2
*
*-----*
* VAPOR GENERATION IN CORE
*
20500500  VGENCORE  SUM    1.0    0.0            1            0
20500501  0.0    1.0    VAPGEN    100010000    1.0    VAPGEN    100020000
+      1.0    VAPGEN    100030000    1.0    VAPGEN    100040000
+      1.0    VAPGEN    100050000    1.0    VAPGEN    100060000
+      1.0    VAPGEN    100070000    1.0    VAPGEN    100080000
+      1.0    VAPGEN    100090000    1.0    VAPGEN    100100000
+      1.0    VAPGEN    100110000
*
* VAPOR CONDENSATION IN STEAM GENERATOR PRIMARY SIDE
*
20500600  VCONDSG  SUM    1.0    0.0            1            0
20500601  0.0    1.0    VAPGEN    162010000    1.0    VAPGEN    164010000
+      1.0    VAPGEN    162020000    1.0    VAPGEN    164020000
+      1.0    VAPGEN    162030000    1.0    VAPGEN    164030000
+      1.0    VAPGEN    162040000    1.0    VAPGEN    164040000
+      1.0    VAPGEN    162050000    1.0    VAPGEN    164050000
+      1.0    VAPGEN    162060000    1.0    VAPGEN    164060000
*
* VAPORIZATION ALONG UPPER PLENUM AND HOT LEG
*
20500800  VGENHLG  SUM    1.0    0.0            1            0
20500801  0.0    1.0    VAPGEN    105010000    1.0    VAPGEN    105020000
+      1.0    VAPGEN    105030000    1.0    VAPGEN    105040000
+      1.0    VAPGEN    110010000    1.0    VAPGEN    125010000
+      1.0    VAPGEN    120010000    1.0    VAPGEN    120020000
+      1.0    VAPGEN    120030000    1.0    VAPGEN    120040000
+      1.0    VAPGEN    140010000    1.0    VAPGEN    140020000
+      1.0    VAPGEN    140030000    1.0    VAPGEN    140040000
+      1.0    VAPGEN    150010000
*
* STEAM CONDENSATION IN COLD LEG SIDE COLLECTOR & FALLING PIPE
*
20500900  VCONDCL  SUM    1.0    0.0            1            0

```

20500901 0.0 1.0 VAPGEN 170010000 1.0 VAPGEN 180010000

\* EXCESS VAPOR GENERATION

20500700	VGENEXCS	SUM	1.0	0.0		1	0
20500701	0.0 1.0	CNTRLVAR 5		1.0	CNTRLVAR 6		
+		1.0 CNTRLVAR 8		1.0	CNTRLVAR 9		

\* HEAT INPUT IN CORE

20502000	QCORE	SUM	1.0	0.0		1	0
20502001	0.0 1.0	Q	100010000		1.0 Q	100020000	
+		1.0 Q	100030000		1.0 Q	100040000	
+		1.0 Q	100050000		1.0 Q	100060000	
+		1.0 Q	100070000		1.0 Q	100080000	
+		1.0 Q	100090000		1.0 Q	100100000	
+		1.0 Q	100110000				

\* HEAT INPUT IN SG SECONDARY SIDE

20502100	QSGSEC	SUM	1.0	0.0	1	0
20502101	0.0 1.0	Q	250010000		1.0 Q	250020000
+		1.0 Q	250030000			

\* EXCESS HEAT INPUT

20502200	QLEXCESS	SUM	1.0	0.0	1	0
20502201	0.0 1.0	CNTRLVAR 20		-1.0	CNTRLVAR 21	

\* HEAT LOSSES AT UPPER PLENUM

20502500	QLOSSUP	SUM	1.0	0.0	1	0
20502501	0.0 1.0	Q	105010000		1.0 Q	105020000
+		1.0 Q	105030000		1.0 Q	105040000
+		1.0 Q	115010000		1.0 Q	115020000
+		1.0 Q	110010000			

\* HEAT LOSSES AT HOT LEG

20502600	QLOSSHL	SUM	1.0	0.0	1	0
20502601	0.0 1.0	Q	120010000		1.0 Q	120020000
+		1.0 Q	120030000		1.0 Q	120040000
+		1.0 Q	140010000		1.0 Q	140020000
+		1.0 Q	140030000		1.0 Q	140040000
+		1.0 Q	125010000			

\* HEAT LOSSES AT COLD LEG

20502700	QLOSSCL	SUM	1.0	0.0	1	0
20502701	0.0 1.0	Q	180010000		1.0 Q	185010000
+		1.0 Q	190010000		1.0 Q	195010000

\* HEAT LOSSES AT DOWNCOMER

20502800	QLOSSDC	SUM	1.0	0.0	1	0
20502801	0.0 1.0	Q	220010000		1.0 Q	220020000
+		1.0 Q	220030000		1.0 Q	220040000
+		1.0 Q	220050000		1.0 Q	220060000
+		1.0 Q	210010000			

SUM OF LOSSES

20502400	QLOSSSUM	SUM	1.0	0.0	1	0
20502401	0.0 1.0	CNTRLVAR 25		1.0	CNTRLVAR 26	



```

*          1.0  CNTRLVAR 27      1.0  CNTRLVAR 28
*
* TOTAL EXCESS HEAT INPUT
*
20502300  QTEXCESS      SUM  1.0      0.0      1      0
20502301  0.0      1.0  CNTRLVAR 22      1.0  CNTRLVAR 24
*
*-----*
*
* HYDRODYNAMIC COMPONENTS:
*
* CORE
*
1000000  CORE  PIPE
1000001  11
1000101  0.00219  11
1000301  0.232      11
1000401  0.0         11
1000601  90.0        11
1000801  5.E-5       7.6E-3  11
1000901  0.41        0.41    10
1001001  00          11
1001101  1000        10
*
* INITIAL VALUES (P, UF, UG, VOIDG)
*
1001201  0  3.4025E5  4.14E5  2.530E6  0.0  0.0  1
1001202  0  3.3800E5  4.30E5  2.530E6  0.0  0.0  2
1001203  0  3.3590E5  4.60E5  2.530E6  0.0  0.0  3
1001204  0  3.3370E5  4.72E5  2.530E6  0.0  0.0  4
1001205  0  3.3150E5  4.88E5  2.530E6  0.0  0.0  5
1001206  0  3.2940E5  5.08E5  2.530E6  0.0  0.0  6
1001207  0  3.2730E5  5.28E5  2.530E6  0.0  0.0  7
1001208  0  3.2516E5  5.43E5  2.530E6  0.0  0.0  8
1001209  0  3.2304E5  5.49E5  2.530E6  0.0  0.0  9
1001210  0  3.2093E5  5.50E5  2.530E6  0.0  0.0  10
1001211  0  3.1883E5  5.50E5  2.530E6  0.0  0.0  11
1001300  1
1001301  0.072      0.0      0.0      10
*
1020000  CORTOUP  SNGI=JN
1020101  10001000 105000000
1020102  1.08E-3  1.9  1.9  1000
1020301  1  0.072  0.0  0.0
*
* UPPER PLENUM, LOWER PART
*
1050000  UPPELOW  PIPE
1050001  4
1050101  0.00312  4
1050301  0.572    4
1050401  0.000    4
1050601  90.0     4
1050801  5.0E-5   0.063  4
1050901  0.0      0.0     3
1051001  00       4
1051101  1000     3
1051201  0  3.151E5  5.50E5  2.530E6  0.0  0.0  1
1051202  0  3.100E5  5.50E5  2.530E6  0.0  0.0  2
1051203  0  3.048E5  5.49E5  2.530E6  0.0  0.0  3
1051204  0  2.996E5  5.49E5  2.530E6  0.0  0.0  4
1051300  1
1051301  C.072    0.0      0.0      3

```

-----\*  
UPPER PLENUM ( TO THE HOT LEG )



```

*
1100000  UPLCONX  BRANCH
1100001  3 1
1100101  0.00312 0.858 0.0 0.0 90.0 0.858 5.0E-5 0.063 00
1100200  0 2.9309E5 5.49E5 2.530E6 0.0
1101101  105010000 110000000 0.00312 0.66 0.66 1000
1102101  110010000 120000000 0.000412 1.22 1.22 1002
1103101  110010000 115000000 0.00312 0.85 0.85 1000
1101201  0.072 0.0 0.0
1102201  0.072 0.0 0.0
1103201  0.0 0.0 0.0

```

\* UPPER PLENUM ( FROM THE HOT LEG )

```

*
1150000  UPLHEAD  PIPE
1150001  2
1150101  0.00312 1
1150102  0.0553 2
1150301  0.414 1
1150302  0.1 2
1150401  0.0 2
1150601  90.0 2
1150801  5.E-5 0.063 1
1150802  5.E-5 0.265 2
1150901  0.16 0.16 1
1151001  00 2
1151101  1100
1151201  0 2.912E5 5.49E5 2.530E6 0.0 0.0 1
1151202  4 2.908E5 415.0 4.0E-4 0.0 0.0 2
1151300  1
1151301  0.0 0.0 0.0 1

```

-----  
\* HOT LEG ( FIRST PART )

```

*
1200000  HTLGDOWN  PIPE
1200001  4 * NUMBER OF VOLUMES
1200101  0.000412 4 * FLOW AREAS
1200301  0.5605 4 * LENGTHS
1200501  0.0 4 * HORIZ. ANGLES
1200601  -50.0 4 -- * VERTICAL ORIENTATION
1200701  -0.4925 4 * ELEVATION CHANGE
1200801  5.0E-5 0.0229 4 * ROUGHNESS, HYDR. DIAMETER
1200901  0.0 0.0 3
1201001  00 4 * VOL FLAGS=FRICITION+NONEQUILIBRIUM
1201101  1000 3 * JUN FLAGS=NOCHOKE,SMOOTH,2VEL,FUL
* VOLUME INITIAL CONDITIONS=PRESSURE, INTERNAL ENERGIES, VAPOUR VOID FRACTION
1201201  0 2.9450E5 5.502E5 2.530E6 0.0 0.0 2
1201202  0 2.9640E5 5.500E5 2.530E6 0.0 0.0 4
* JUNCTION INITIAL CONDITIONS=MASS FLOWS
1201300  1
1201301  0.072 0.0 0.0 3

```

\* HOT LEG ( CONNECTION TO THE PRESSURISER )

\*\*\*\*\* PRESSURIZER REMOVED BY JT

```

*
1250000  HTLGFLAT  BRANCH
1250001  2 1 * NO OF JUN, INIT=MFLOW
1250101  0.412E-3 0.559 0.0 0.0 0.0 0.0 5.0E-5 0.0229 00
1250200  0 2.907E5 5.49E5 2.530E6 0.0
* CONNECTIONS
1251101  120010000 125000000 4.12E-4 0.36 0.36 1000
1252101  125010000 140000000 4.12E-4 0.36 0.36 1000
* JUNCTION INITIAL CONDITIONS: MFLOWL, MFLOWG, INTERPHASE
1251201  0.072 0.0 0.0
1252201  0.072 0.0 0.0

```

\* HOT LEG ( TO THE STEAM GENERATOR )

```

*
1400000    HOTLEGUP    PIPE
1400001    4
1400101    4.12E-4      4
1400301    0.580        4
1400501    0.0          4
1400601    90.0         4
1400701    0.580        4
1400801    5.0E-5    0.0229  4
1400901    0.0          0.0    3
1401001    00           4
1401101    1000        3
* INITIAL CONDITIONS
1401201    0    2.959E5    5.490E5    2.530E6    0.0    0.0    2
1401202    0    2.950E5    5.490E5    2.530E6    0.0    0.0    4
1401300    1
1401301    0.072      0.0    0.0    3

```

-----

\* STEAM GENERATOR, EXTENDED VERSION 2/JH 1.9.87

\* HOT LEG SIDE COLLECTOR (2 BRANCHES WITH CROSSFLOW JUNCTIONS TO SG TUBES)

```

*
1500000    HOTCOLLW    BRANCH
1500001    3    1    * NO OF JUNS, INIT=FLows
* GEOMETRY
1500101    2.043E-3    0.200    0.0    0.0    90.0    0.200
+          5.0E-5    0.051    00
* VOLUME INITIAL CONDITIONS: PRESS, UF, UG, VOIDG
1500200    0    2.985E5    5.520E5    2.530E6    0.0
* CONNECTIONS
1501101    140010000    150000000    4.12E-4    2.5    3.1    1000
1502101    150000000    162000000    7.96E-4    3.7    2.1    1002
1503101    150010000    154000000    2.043E-3    1.3    1.3    1000
* JUNCTION INITIAL CONDITIONS: MFLOWL, MFLOWG, INTERPHASE
1501201    0.072      0.0      0.0
1502201    0.030      0.0      0.0
1503201    0.042      0.0      0.0

```

```

*
1540000    HOTCOLUP    BRANCH
1540001    1    1    * NO OF JUNS, INIT=FLows
* GEOMETRY
1540101    2.043E-3    0.120    0.0    0.0    90.0    0.120
+          5.0E-5    0.051    00
* VOLUME INITIAL CONDITIONS: PRESS, UF, UG, VOIDG
1540200    0    2.970E5    5.520E5    2.530E6    0.0
* CONNECTIONS
1541101    154000000    164000000    7.96E-4    3.7    2.1    1002
* JUNCTION INITIAL CONDITIONS: MFLOWL, MFLOWG, INTERPHASE
1541201    0.042      0.0      0.0

```

\* STEAM GENERATOR, PRIMARY SIDE TUBING (2 PIPES)

```

*
1620000    SGPRIBOT    PIPE
1620001    6    * NO OF PIPE VOLUMES
1620101    0.7964E-3    6    * AREAS
1620301    0.762        2    * LENGTHS
1620302    2.313        4
1620303    0.762        6
1620501    90.0         3    * HORIZ ANGLES (U-TUBE)
1620503    -90.0        6
1620601    0.0          6    * VERTIC ANGLES
1620701    0.0          6    * ELEV CHANGES

```

1620801 5.0E-5 0.013 6 \* FRICTION DATA  
 1620901 0.0 0.0 2 \* JUNCTION LOSS COEFF  
 1620902 0.11 0.11 3  
 1620903 0.0 0.0 5  
 1621001 00 6 \* VOL FLAGS: FRIC+NONEQ  
 1621101 1070 5 \* JUN FLAGS: NOCHOK, SMOOTH, 2VEL, CENTRAL  
 \* INITIAL VOLUME CONDITIONS: PRESS, UF, UG, VOIDG  
 1621201 0 2.985E5 5.01E5 2.530E6 0.0 0.0 1  
 1621202 0 2.985E5 4.67E5 2.530E6 0.0 0.0 2  
 1621203 0 2.985E5 4.38E5 2.530E6 0.0 0.0 3  
 1621204 0 2.985E5 4.28E5 2.530E6 0.0 0.0 4  
 1621205 0 2.985E5 4.26E5 2.530E6 0.0 0.0 5  
 1621206 0 2.985E5 4.25E5 2.530E6 0.0 0.0 6

\* INITIAL JUNCTION CONDITIONS  
 1621300 1 \* FLOWS FOLLOW  
 1621301 0.030 0.0 0.0 5

\*  
 1640000 SGPRITOP PIPE  
 1640001 6 \* NO OF PIPE VOLUMES  
 1640101 0.7964E-3 6 \* AREAS  
 1640301 0.762 2 \* LENGTHS  
 1640302 2.313 4  
 1640303 0.762 6  
 1640501 90.0 3 \* HORIZ ANGLES  
 1640503 -90.0 6  
 1640601 0 6 \* VERTIC ANGLES  
 1640701 0.0 6 \* ELEV CHANGES  
 1640801 5.0E-5 0.013 6 \* FRICTION DATA  
 1640901 0.7 0.7 2 \* JUNCTION LOSS COEFF  
 1640902 2.11 2.11 3  
 1640903 0.7 0.7 5  
 1641001 00 6 \* VOL FLAGS: FRIC+NONEQ  
 1641101 1000 5 \* JUN FLAGS: NOCHCKE, SMOOTH, 2VEL, FULL I

\* INITIAL VOLUME CONDITIONS: PRESS, UF, UG, VOIDG  
 1641201 0 2.870E5 5.47E5 2.530E6 0.0 0.0 1  
 1641202 0 2.870E5 4.96E5 2.530E6 0.0 0.0 2  
 1641203 0 2.870E5 4.48E5 2.530E6 0.0 0.0 3  
 1641204 0 2.870E5 4.32E5 2.530E6 0.0 0.0 4  
 1641205 0 2.870E5 4.29E5 2.530E6 0.0 0.0 5  
 1641206 0 2.870E5 4.26E5 2.530E6 0.0 0.0 6

\* INITIAL JUNCTION CONDITIONS  
 1641300 1 \* FLOWS FOLLOW  
 1641301 0.042 0.0 0.0 5

\* COLD LEG SIDE COLLECTOR

\*  
 1700000 COLDCOLL BRANCH  
 1700001 3 1 \* NO OF JUNS, INIT=FLWS  
 \* GEOMETRY  
 1700101 2.043E-3 0.200 0.0 0.0 -90.0 -0.200  
 + 5.0E-5 0.051 00

\* VOLUME INITIAL CONDITIONS: PRESS, UF, UG, VOIDG  
 1700200 0 2.885E5 4.266E5 2.530E6 0.0

\* CONNECTIONS  
 1701101 170010000 180000000 4.12E-4 3.1 2.5 1000  
 1702101 162010000 170000000 7.96E-4 2.3 4.1 1001  
 1703101 174010000 170000000 2.043E-3 1.3 1.3 1000

\* JUNCTION INITIAL CONDITIONS: MFLOWL, MFLOWG, INTERPHASE  
 1701201 0.072 0.0 0.0  
 1702201 0.030 0.0 0.0  
 1703201 0.042 0.0 0.0

\*  
 1740000 COLDCOLL BRANCH  
 1740001 1 1 \* NO OF JUNS, INIT=FLWS  
 \* GEOMETRY  
 1740101 2.043E-3 0.120 0.0 0.0 -90.0 -0.120

```

*          5.0E-5      0.051      00
* VOLUME INITIAL CONDITIONS: PRESS, UP, UG, VOIDG
1740200      0      2.870E5      4.245E5      2.530E6      0.0
* CONNECTIONS
1741101      164010000      174000000      7.96E-4      2.3      4.1      1001
* JUNCTION INITIAL CONDITIONS: MFLOWL, MFLOWG, INTERPHASE
1741201      0.042      0.0      0.0

```

```

*-----
* COLD LEG

```

```

*
1800000      CLGUP      SNGLVOL
* GEOMETRY
1800101      4.12E-4      2.32      0.0      0.0      -90.0      -2.32
+          5.0E-5      0.0229      00

```

```

* INITIAL COND
1800200      0      4.401E5      4.24E5      2.530E6      0.0

```

```

*
1830000      COLDLEG1      SNGLJUN
1830101      180010000      185000000
1830102      0.0      0.6      0.6      1000
1830201      1      0.072      0.0      0.0

```

```

*
1850000      CLGRISE      SNGLVOL
1850101      4.12E-4      2.30      0.0      0.0      60.0
1850102      2.0      5.00E-5      0.0      00
1850200      0      3.014E5      4.23E5      2.530E6      0.0

```

```

*
1870000      COLDLEG2      SNGLJUN
1870101      185010000      190000000
1870102      0.0      0.6      0.6      1000
1870201      1      0.072      0.0      0.0

```

```

*
1900000      CLCDOWN      ENGLVOL
1900101      4.12E-4      1.41      0.0      0.0      -90.0
1900102      -1.41      5.0E-5      0.0      00
1900200      0      3.085E5      4.21E5      2.530E6      0.0

```

```

*
1930000      COLDLEG3      SNGLJUN
1930101      190010000      195000000
1930102      0.0      0.6      0.6      1000
1930201      1      0.072      0.0      0.0

```

```

*
1950000      CLGFLAT      SNGLVOL
1950101      4.12E-4      3.40      0.0      0.0      0.0
1950102      0.0      5.0E-5      0.0      00
1950200      0      3.050E5      4.19E5      2.530E6      0.0

```

```

*-----
* DOWNCOMER ( UPPER PART )

```

```

*
*2050000      DCMRHEAD      SNGLVOL
*2050101      8.04E-4      0.61      0.0      0.0      90.0
*2050102      0.61      5.0E-5      0.0      00
*2050200      0      4.336E5      4.20E5      2.550E6      0.0

```

```

* DOWNCOMER ( CONNECTION TO THE COLD LEG )

```

```

*
2100000      DCMRCONX      BRANCH
2100001      2      1
2100101      8.04E-4      1.22      0.0      0.0      -90.0
2100102      -1.22      5.0E-5      0.0      00
2100200      0      3.049E5      4.18E5      2.530E6      0.0
2101101      195010000      210000000      0.0      1.42      1.42      1001
2102101      210010000      220000000      0.0      0.94      0.94      1000
*2103101      210000000      205000000      0.0      0.2      0.2      1000

```



2101201	0.072	0.0	0.0
2102201	0.072	0.0	0.0

\*  
\* DOWNCOMER  
\*

2200000	DOWNCOMR	PIPE					
2200001	6						
2200101	0.804E-3	4					
2200105	1.225E-3	6					
2200301	1.0945	1					
2200302	1.22275	3					
2200305	1.283	6					
2200601	-90.0	6					
2200801	5.0E-5	0.032	4				
2200802	5.0E-5	0.0395	6				
2200901	0.0	0.0	5				
2201001	00	6					
2201104	1000	5					
2201201	0	3.158E5	4.177E5	2.530E6	0.0	0.0	1
2201202	0	3.256E5	4.167E5	2.530E6	0.0	0.0	2
2201203	0	3.381E5	4.157E5	2.530E6	0.0	0.0	3
2201204	0	3.498E5	4.146E5	2.530E6	0.0	0.0	4
2201205	0	3.619E5	4.136E5	2.530E6	0.0	0.0	5
2201206	0	3.740E5	4.125E5	2.530E6	0.0	0.0	6
2201300	1						
2201301	0.072	0.0	0.0	5			

\*-----  
\* LOWER PLENUM  
\*

\* NEW LOWER PLENUM  
\*

2300000	LPFLAT2	BRANCH							
2300001	2	1							
2300101	1.83E-3	0.740	0.0	0.0	0.0	0.0	5.0E-5	0.0	00
2300200	0	3.80E5	4.126E5	2.53E6	0.0				
2301101	220010000	230000000	0.0	0.89	0.89	1000			
2302101	230010000	240000000	0.0	0.29	0.29	1000			
2301201	0.072	0.0	0.0						
2302201	0.72	0.0	0.0						

\*  
\* LOWPLUP  
\* PIPE

2400000	4							
2400001	4							
2400101	4.083E-3	2						
2400102	2.736E-3	4						
2400301	1.20	1						
2400302	1.20	2						
2400303	0.684	3						
2400304	0.826	4						
2400601	90.0	4						
2400801	5.0E-5	0.0	4					
2400901	0.63	0.63	1					
2400902	3.63	3.63	3					
2401001	00	4						
2401101	1000	3						
2401201	0	3.743E5	4.129E5	2.530E6	0.0	0.0	1	
2401202	0	3.631E5	4.134E5	2.530E6	0.0	0.0	2	
2401203	0	3.533E5	4.137E5	2.530E6	0.0	0.0	3	
2401204	0	3.452E5	4.139E5	2.530E6	0.0	0.0	4	
2401300	1							
2401301	0.072	0.0	0.0	3				

\* JUNCTION LOSS COEFF.

2450000	LPTOCORE	SNGLJUN			
2450101	240010000	100000000			
2450102	0.0	0.87	1.87	1000	
2450201	1	0.072	0.0	0.0	

-----  
 \* STEAM GENERATOR SECONDARY SIDE  
 \* (PIPE OF 3 COMPONENTS, SINGLJUN, TMDPVOL)

2500000	SGSEC	PIPE							
2500001	3								* NO OF VOLS
2500101	0.7501		2						* FLOW AREAS
2500102	0.8302		3						
2500301	0.120		2						* HEIGHTS
2500302	0.166		3						
2500601	90.0		5						* VERTICAL ANGLES
2500801	5.0E-5	0.0	3						* ROUGHNESS, DRY
2500901	1.3	1.3	2						* JUNCTION LOSSES
2501001	00		3						* VOL FLAGS: FRICT, NON-EQUIL
2501101	1000		2						* JUN FLAGS: NOCHOKE, SMOOTH, 2VEL, IN
2501201	2	1.035E5	1.5E-5	0.0					
2501202	2	1.023E5	6.9E-4	0.0	0.0	0.0	3		* INITIAL VOL COND: PRESS, STAT X
2501300	0								* INITIAL JUN COND:
2501301	0.0	0.0	0.0	2					* VELOCITIES

2560000	SECTOBY	SINGLJUN							
2560101	250010000	260000000	0.05	10.0	5.0	1100			
2560201	0	0.00	0.00	0.0					

2600000	SECBRY	TMDPVOL							
2600101	1.0	0.20	0.0	0.0	0.0	0.0	5.0E-5	0.0	10
2600200	2								
2600201	0.0	1.02E5	0.0007						

-----  
 \* LEAK JUNCTION

3000000	LEAK	SINGLJUN							
3000101	230000000	310000000	9.2E-4	10.0	10.0	1000			
3000201	0	0.0	0.0	0.0					
3000200	0								
3000201	0.0	0.0	0.0	0.0					

\* LEAK BOUNDARY

3100000	LEAKBDRY	TMDPVOL							
3100101	1.0E-3	0.5	0.0	0.0	0.0	0.0	5.7E-5	0.0	00
3100200	0	0	UF	220060000					
3100201	4.00E5	3.9E5	4.00E5	2.533E6	0.0				
3100202	4.30E5	3.9E5	4.30E5	2.533E6	0.0				

-----  
 \* HEAT STRUCTURES

\* STEAM GENERATOR TUBES (2 SIMILAR STRUCTURES  
 WITH DIFFERENT BOUNDARY VOLUMES)

\* LOWER PART

11621000	6	3	2	1	6.5E-3				
11621100	0	1							* MESH LOC FLAG, MESH FORMAT FLAG
11621101	2	7.5E-3							* NO OF INTERVALS, RIGHT BDRY COORD
11621201	3	2							* COMPOSITION NO, INTERVAL NO
11621301	0.0	2							* SOURCE TERM, -"



11621400 0 \* INITIAL COND FLAG: TEMPERATURES FOLLOW  
 11621401 375.0 1 \* MESH POINT TEMPERATURES  
 11621402 374.0 2  
 11621403 374.0 3

\* LEFT HYDROD BDRY VOLUME, INCR, BDRY=CONV, SURF AREA FLG -VAL, STR NO  
 11621501 162010000 10000 1 1 4.5720 2  
 11621502 162030000 10000 1 1 13.878 4  
 11621503 162050000 10000 1 1 4.5720 6

\* RIGHT (AS LEFT)  
 11621601 250010000 0 1 1 4.5720 2  
 11621602 250010000 0 1 1 13.878 4  
 11621603 250010000 0 1 1 4.5720 6

11621701 0 0.0 0.0 0.0 6 \* NO INTERNAL SOURCE

\* LEFT BDRY DATA: CHF FLAG, DHY, HEATED EQJ. DIAM LENGTH

11621801 0 0.013 0.013 0.762 2  
 11621802 0 0.013 0.013 2.313 4  
 11621803 0 0.013 0.013 0.762 6

\* RIGHT AS LEFT  
 11621901 0 0.015 0.015 0.762 2  
 11621902 0 0.015 0.015 2.313 4  
 11621903 0 0.015 0.015 0.762 6

\* UPPER PART  
 11641000 6 3 2 1 6.5E-3  
 11641100 0 1  
 11641101 2 7.5E-3  
 11641201 3 2  
 11641301 0.0 2  
 11641400 0

11641401 375.0 1  
 11641402 374.0 2  
 11641403 374.0 3  
 11641501 164000000 10000 1 1 4.5720 2  
 11641502 164030000 10000 1 1 13.878 4  
 11641503 164050000 10000 1 1 4.5720 6  
 11641601 250020000 0 1 1 4.5720 2  
 11641602 250020000 0 1 1 13.878 4  
 11641603 250020000 0 1 1 4.5720 6

11641701 0 0.0 0.0 0.0 6  
 11641801 0 0.013 0.013 0.762 2  
 11641802 0 0.013 0.013 2.313 4  
 11641803 0 0.013 0.013 0.762 6  
 11641901 0 0.015 0.015 0.762 2  
 11641902 0 0.015 0.015 2.313 4  
 11641903 0 0.015 0.015 0.762 6

\*-----\*  
 \* FUEL RODS:  
 \* CORE (MgO) + CLADD. LG (S-STEEL)  
 \*

	NSTR	NP	CYL	STDY=YES	LEFT COCRD
11003000	11	5	2	1	0.0
11003100	0	1			* MESH LOC = ENTER HERE
11003101	3	3.55E-3			* NO OF INTERVALS, RIGHT COORDINATE
11003102	1	4.55E-3			
11003201	2	3			* COMPOSITION 2 (MGO) / FIRST 3 INTERVALS
11003203	1	4			* COMPOSITION 1 (STEEL) / 4TH INTERVAL
11003301	0.0	1			* SOURCE = 1.0 IN MID-MGO, 0.0 ELSEWHERE
11003302	1.0	2			
11003303	0.0	4			
11003400	-1				* INIT. TEMP FLAG = ALL STRS SEPARATELY

\* MESH POINT TEMPS FOR ALL HEAT STRUCTURES  
 11003401 372.27 372.27 372.27 372.27 372.27  
 11003402 383.26 383.26 382.34 381.02 380.70  
 11003403 397.29 397.29 395.25 392.32 391.64

11003404	409.18	409.18	406.32	402.23	401.30	
11003405	422.07	422.07	418.37	413.07	411.88	
11003406	429.58	429.58	425.67	420.08	418.85	
11003407	434.09	434.09	430.32	424.93	423.76	
11003408	434.34	434.34	431.16	426.61	425.63	
11003409	430.29	430.29	428.11	424.97	424.29	
11003410	422.87	422.87	421.91	420.51	420.21	
11003411	415.07	415.07	415.07	415.07	415.07	
11003501	0	0	1	0.0	11	* LEFT BDRY DATA
11003601	100010000	10000	1	1	4.408	11 * RIGHT --
11003701	100	0.0	0.0	0.0	1	* SOURCE DISTRIBUTION
11003702	100	0.0407	0.0	0.0	2	
11003703	100	0.0887	0.0	0.0	3	
11003704	100	0.1221	0.0	0.0	4	
11003705	100	0.1559	0.0	0.0	5	
11003706	100	0.1628	0.0	0.0	6	
11003707	100	0.1559	0.0	0.0	7	
11003708	100	0.1313	0.0	0.0	8	
11003709	100	0.0908	0.0	0.0	9	
11003710	100	0.0406	0.0	0.0	10	
11003711	100	0.0	0.0	0.0	11	
11003801	0	0.0	0.0	0.232	11	* LEFT EXTRA DATA
11003901	0	7.6E-3	3.1E-3	0.232	11	* RIGHT --

\* CORE HOUSING (EXTERNAL HEATERS)  
\*

	NSTR	NP	RECT	STDY=YE3	LEFT COORD	
11005000	9	3	1	1	0.0	
11005100	0	1				* MESH LOC = ENTER HERE
11005101	2	1.0E-3				* NO OF INTERVALS, RIGHT COORDINATE
11005203	1	2				* COMPOSITION 1 (STEEL)
11005301	0.0	2				* NO (RADIAL) SOURCE
11005400	-1					* INIT. TEMP FLAG: SEPARATE FOR ALL STRS
11005401	389.32		391.02		392.72	
11005402	393.14		394.85		396.52	
11005403	398.02		399.70		401.39	
11005404	404.00		405.68		407.35	
11005405	410.23		411.90		413.57	
11005406	416.24		417.90		419.57	
11005407	421.44		423.10		424.76	
11005408	425.34		426.49		428.65	
11005409	427.61		429.27		430.92	

\* LEFT BDRY DATA

11005501	100020000	10000	1	0	0.03762	9
----------	-----------	-------	---	---	---------	---

\* RIGHT BDRY DATA (VOL 310010000 IS USED AS A DUMMY VOLUME)  
\* WITH FIXED HEAT FLUX FROM TABLE 101

11005601	310010000	0	2101	0	0.03762	9
----------	-----------	---	------	---	---------	---

\* NO (AXIAL) SOURCE

11005701	0	0.0	0.0	0.0	9	
----------	---	-----	-----	-----	---	--

\* LEFT EXTRA DATA

11005801	0	7.6E-3	0.0	0.232	9	
----------	---	--------	-----	-------	---	--

\* UPPER PLENUM (ENVIRONMENTAL LOSSES)  
\*

	NSTR	NMP	CYL	STDY=Y	LEFT COORD	
11101000	7	5	2	1	0.0315	
11101100	0	1				* MESH LOC & FORMAT
11101101	2	0.034				* INTERVALS RIGHT COORD
11101102	2	0.100				
11101201	1	2				* COMPOSITION, INTERVALS
11101202	4	4				
11101301	0.0	4				* RADIAL SOURCE DISTRIB
11101401	413.3	1				* INITIAL TEMPERATURES
11101403	413.2	3				

```

11101404 340.7 4
11101405 297.2 5
* LEFT BOUNDARY DATA
11101501 105010000 10000 1 1 0.572 4
11101502 110010000 0 1 1 0.858 5
11101503 115010000 10000 1 1 0.414 7
* RIGHT BOUNDARY
11101601 -200 0 3110 1 0.572 4
11101602 -200 0 3110 1 0.858 5
11101603 -200 0 3110 1 0.414 7
* AXIAL SOURCE
11101701 0 0.0 0.0 0.0 7
* ADDITIONAL LEFT BOUNDARY DATA
11101801 0 0.063 0.063 0.0 7
*
* HOT LEG (ENVIRONMENTAL LOSSES)
*
* NSTR NMP CYL STDY=Y LEFT COORD
11201000 9 5 2 1 0.01145
11201100 0 1 * MESH LOC & FORMAT
11201101 2 0.01345 * INTERVALS, RIGHT COORD
11201102 2 0.0635
11201201 1 2 * COMPOSITION, INTERVALS
11201202 4 4
11201301 0.0 4 * RADIAL SOURCE DISTRIB
11201401 413.1 3 * INITIAL TEMPERATURES
11201402 336.6 4
11201403 297.7 5
* LEFT BOUNDARY DATA
11201501 120010000 10000 1 1 0.5685 4
11201502 125010000 0 1 1 0.559 5
11201503 140010000 10000 1 1 0.580 9
* RIGHT BOUNDARY
11201601 -200 0 3110 1 0.5685 4
11201602 -200 0 3110 1 0.559 5
11201603 -200 0 3110 1 0.580 9
* AXIAL SOURCE
11201701 0 0.0 0.0 0.0 9
* ADDITIONAL LEFT BOUNDARY DATA
11201801 0 0.0229 0.0229 0.0 9
*
* COLD LEG (ENVIRONMENTAL LOSSES)
*
* NSTR NMP CYL STDY=Y LEFT COORD REFLOOD=NO
11901000 4 5 2 1 0.01145 0
11901100 1201 * MESH DATA EQUAL TO HOT LEG
11901401 374.4 3
11901402 322.3 4
11901403 296.2 5
* LEFT BOUNDARY DATA
11901501 180010000 0 1 1 2.320 1
11901502 185010000 0 1 1 2.300 2
11901503 190010000 0 1 1 1.410 3
11901504 195010000 0 1 1 3.400 4
* RIGHT BOUNDARY
11901601 -200 0 3120 1 2.320 1
11901602 -200 0 3120 1 2.300 2
11901603 -200 0 3120 1 1.410 3
11901604 -200 0 3120 1 3.400 4
* AXIAL SOURCE
11901701 0 0.0 0.0 0.0 4
* ADDITIONAL LEFT BOUNDARY DATA
11901801 0 0.063 0.063 0.0 4
*
* DOWNCOMER
*

```

```

*          NSTR  NMP   CYL  STDY-Y   LEFT COORD
12201000   7    5     2     1     0.019
12201100   0    1           * MESH LOC & FORMAT
12201101   2    0.21       * INTERVALS, RIGHT COORD
12201102   2    0.071
12201201   1    2           * COMPOSITION, INTERVALS
12201202   4    4
12201301   0.0  4           * RADIAL SOURCE DISTRIB
12201401   372.1 3           * INITIAL TEMPERATURES
12201402   324.0 4
12201403   296.5 5
* LEFT BOUNDARY DATA
12201501   210010000       0    1    1    1.220    1
12201502   220010000       0    1    1    0.880    2
12201503   220020000     10000  1    1    1.22275  4
12201504   220040000     10000  1    1    1.2830   7
* RIGHT BOUNDARY
12201601   -200           0  3120  1    1.220    1
12201602   -200           0  3120  1    0.880    2
12201603   -200           0  3120  1    1.22275  4
12201604   -200           0  3120  1    1.2830   7
* AXIAL SOURCE
12201701   0    0.0    0.0    0.0    7
* ADDITIONAL LEFT BOUNDARY DATA
12201801   0    0.0380  0.0380  0.0    7
*
*-----
*
* COMPOSITION TABLES
*
*-----
* MATERIAL PROPERTIES FOR COMPOSITION 1, CLADDING & CORE SHROUD
*
20100100  TBL/FCTN    1    1
* THERMAL CONDUCTIVITY
20100101  293.15    14.2
20100102  323.15    15.5
20100103  373.15    16.0
20100104  573.15    18.3
20100105  723.15    21.0
20100106  973.15    24.1
20100107 1173.15    27.6
* VOLUMETRIC HEAT CAPACITY
20100151  293.15    3.718E6
20100152  323.15    3.763E6
20100153  373.15    4.069E6
20100154  573.15    4.408E6
20100155  773.15    4.748E6
20100156 1273.15    5.027E6
*
*-----
* MATERIAL PROPERTIES OF MGO, COMPOSITION 2
20100200  TBL/FCTN    1    1
* THERMAL CONDUCTIVITY
20100201  273.15    7.10
20100202  473.15    5.48
20100203  673.15    3.85
20100204  723.15    3.46
20100205  773.15    3.18
20100206  823.15    2.98
20100207  873.15    2.82
20100208  923.15    2.68
20100209  973.15    2.57
*
* VOLUMETRIC HEAT CAPACITY
20100251  273.15    3.300E6

```



20100252	293.15	3.300E6
20100253	573.15	3.296E6
20100254	673.15	3.323E6
20100255	723.15	3.314E6
20100256	923.15	3.865E6
20100257	973.15	3.884E6

\*

\* -----  
\* PROPERTIES OF COMPOSITION 3, STEAM GENERATOR TUBES, COPPER

\*

	TYPE	COND = TABLE	VOLUM. CP = TABLE
20100300	TBL/FCTN	1	1

\*

\* THERMAL CONDUCTIVITY (ASSUMED CONSTANT)

20100301 385.0

\*

\* VOLUMETRIC HEAT CAPACITY (ASSUMED CONSTANT)

20100351 3.435E6

\*

\* -----  
\* COMPOSITION 4, MINERAL WOOL, LEG OUTER INSULATOR

\*

20100400	TBL/FCTN	1	1
----------	----------	---	---

\* CONDUCTIVITY

20100401 0.16

\* VOLUMETRIC HEAT CAPACITY

20100451 2.1E5

\*

\* =====

\*

\* GENERAL TABLES: POWERS &amp; LOSS BOUNDARY HEAT TRANSFER COEFFICIENTS

\*

\* - FUEL RODS

20210000 POWER

20210002 0.0 12.0E3

20210004 1.0E4 12.0E3

\*

\* - EXTERNAL HEATERS, 5 KW = 13.8 KW/M2

20210100 HTRNRATE

20210102 0.0 -13.8E3

20210104 1.0E4 -13.8E3

\*

\* UPPER PLENUM &amp; HOT LEG

20211000 HTC-T

20211001 0.0 6.1

20211002 1.0 26.1

20211003 1.0E4 26.1

\*

\* COLD LEG &amp; DOWNCOMER

20212000 HTC-T

20212001 0.0 6.1

20212002 1.0 26.1

20212003 1.0E4 26.1

\*

\* ENVIRONMENT TEMPERATURE

20220000 TEMP

20220001 0.0 293.0

20220002 1.0E4 293.0

\*

\* \* ===== \* END OF INPUT =====

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(See instructions on the reverse)

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10. SUPPLEMENTARY NOTES

11. ABSTRACT (200 words or less)

Natural circulation experiments carried out in the REWET-III facility in 1985 have been used for RELAP5/MOD2 assessment. The REWET-III facility is a scaled-down model of VVER-440 type reactors. The facility consists of a pressure vessel in which the downcomer is simulated with an external pipe assembly, hot and cold legs with loop seals and a horizontal steam generator. The volume scaling factor compared to the reference reactor is 1:2333. The present paper summarizes the experiences gained in the RELAP5/MOD2 calculations of selected REWET-III single- and two-phase natural circulation experiments. The code's ability to represent the main phenomena of experiments in both cases was satisfactory.

12. KEY WORDS/DESCRIPTORS (List words or phrases that will assist researchers in locating the report.)

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ASSESSMENT OF RELAP5/MOD2 AGAINST NATURAL CIRCULATION  
EXPERIMENTS PERFORMED WITH THE REWET-III FACILITY

APRIL 1992