

International Agreement Report

Assessment of RELAP5/MOD2, Cycle 36.04 Against LOFT Small Break Experiment L3-5

Prepared by
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Office of Nuclear Regulatory Research
U.S. Nuclear Regulatory Commission
Washington, DC 20555

March 1992

Prepared as part of
The Agreement on Research Participation and Technical Exchange
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ICAP
ASSESSMENT OF RELAP5/MOD2, Cycle 36.04
AGAINST LOFT SMALL BREAK EXPERIMENT
L3-5

ABSTRACT

The LOFT small break experiment L3-5 has been analyzed using the RELAP5/MOD2 code. The code version used, Cycle 36.04, is a frozen version of the code.

Three calculations were carried out in order to study the sensitivity to changes of steam generator modelling and of core bypass flow. The differences between the calculations and the experiment have been quantified over intervals in real time for a number of variables available from the experiment.

Approved by

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1 INTRODUCTION

An International Thermal-Hydraulic Code Assessment and Applications Program (ICAP) is at present being conducted by several countries under the auspices of the USNRC (1). The goal of the program is to make quantitative statements regarding the prediction capabilities of current best-estimate thermal-hydraulic computer codes. Such codes have been used for many years as state-of-the-art instruments to study and verify numerical and correlative computational models with experimental results. Some of these codes have reached a high degree of sophistication. They include models for all processes which are essential to thermal-hydraulic scenarios in the nuclear power reactor application. So far, however, these codes have not achieved status as reactor licensing tools, i.e. they do not fulfill the Appendix K rules (2), although they are often applied to other calculations. The present ICAP aims to quantify uncertainties in the codes so that the codes may be used for licensing purposes.

Sweden's contributions to ICAP encompass assessment calculations using the two thermal-hydraulic codes TRAC-PF1/MOD1 (3) and RELAP5/MOD2 (4). The work is conducted by Studsvik Energiteknik AB and is sponsored by the Swedish Nuclear Power Inspectorate.

A data package on tape containing input files and predicted data has been produced. The content is described in Appendix D. A copy of this tape is submitted to USNRC as a part of the ICAP agreement.

2 FACILITY AND TEST DESCRIPTION

The LOFT-experiment series L3 was designed to provide large-scale blowdown system data for PWR small break transients. As part of the Swedish ICAP contribution two experiments out of the L3 series were assigned. In the experiment treated in this report, the LOFT L3-5, the main circulation pumps were stopped shortly after the break was opened. In the other experiment, the LOFT L3-6, see (7), the pumps were allowed to operate at normal speed throughout the test in order to provide data for analyzing the differences in the two-phase scenarios between the two tests. Apart from the difference in pump operational mode the two experiments were nominally identical.

This chapter shall briefly describe the test facility, the L3-5 experiment, the assessment parameters used and some aspects of the measurement uncertainties as well as experimental data separation.

2.1 Test Facility

The objective of the LOFT experiments was to demonstrate thermal-hydraulic phenomena which might occur in commercial PWR systems during abnormal situations. The facility is capable of performing a variety of operational transients and LOCAs. Brief descriptions of the LOFT are given in a number of experiment reports such as (5). The most thorough description is provided by Reeder (6). Only particular design features and characteristics relevant to the L3-5 experiment will be discussed in the following sections.

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A general view of LOFT is shown in Figure 1. In the L3-5 small break experiment the two isolation valves on the broken loop legs were closed so as to prevent the passage of fluid via the header to the suppression vessel.

The break was simulated by a 205.6 mm² orifice in a T-branch line from the intact loop cold leg near the reactor vessel. The aim of the break configuration was to simulate an equally placed 4-in diameter small break on a four-loop 1000 MW(e) PWR.

During the L3-5 experiment the only primary coolant injection was carried out by the HPIS into the reactor vessel downcomer. The experiment was terminated before the LPIS pressure set point was reached.

2.2 The Experiment

After approximately 45 h of nuclear heating the initial conditions listed in Table 1 were obtained. The sequence of events which occurred during this experiment is listed in Table 2. Main imposed actions during the experiment were:

- a. At the time of reactor scram (which for safety reasons had to be verified before the break) the steam generator feed water and steam line valves started to close.
- b. The two main circulation pumps were manually tripped just after the break. Pump coastdown was assumed to end at 750 r/min when the speed control carried out by the motor-generator driving unit was disconnected.

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- c. The HPIS injection started at 13.2 MPa.
- d. The steam generator auxiliary feed was initiated and terminated manually.

2.3 Assessment Parameters

The selection of the appropriate assessment parameters for the LOFT L3-5 experiment, Table 3, followed the recommendations of the ICAP Guidelines (1). The selection was made during the input preparation, since a number of expanded Edit/Plot variables from RELAP5/MOD2 calculations are not available from the restart file but must be saved as control variables.

In some cases liquid level data are compared as pressure differences. For the upper plenum and downcomer levels only bubble plot data shown in (5) were available. These plots were converted into slightly smoothed elevation histories. Due to ambiguous bubble plot data the indicated level behaviour is rather uncertain.

The early break flow was not qualified until 40 s after the break, and showed rather large errors during the remainder of the transient. Comparisons of mass inventory obtained through flow integration were therefore not carried out. For the energy balance, the steam generator heat transfer was not known, and could not even be estimated by the steam produced.

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2.4 Measurement Uncertainty

The instrumentation involves a variety of transducers which may have different accuracies for the same kinds of quantities (5,6). Table 4 is a summary of the accuracies of the measured quantities.

2.5 Experimental Data Preparation

The preparation of the experimental data for plotting and uncertainty analysis required several steps of manipulation of the information. First of all, the data were copied from the original blocked tape files to the CDC standard display code.

A program, LOFTDEC, was developed to sort out the keyword and channel information to be used in the assessment work. The program also decimated the channel data by averaging over time intervals so that information was copied to an intermediate channel information file only every 2nd second up to 200 s after the break, and then every 5th second.

A program, R5SILFT, was developed to select data for desired channels from the intermediate data file. These data were transformed into a new file with the same format as a REIAP5 restart file. Experimental and predicted data could later on be similarly used in plotting and assessment.

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3 CODE AND MODEL DESCRIPTION

The assessment calculations with RELAP5/MOD2 for the LOFT L3-5 experiment were carried out using the cycle 36.04 code version. The code was implemented in June 1986 on a CDC 170-810 computer. The calculational model was based on available LOFT input files and listings. Some changes in the input model were introduced as a result of findings in the L3-5 experiment.

3.1 Code Features

The descriptive document available for the RELAP5/MOD2 code is a rather detailed code manual (4). The main characteristics of the code are summarised in Table 5. A new feature of RELAP5/MOD2 is the cross junction which, according to code manual recommendations, was applied at the steam separator upstream volume and at the hot leg and cold leg vessel junctions.

3.2 Input Model

The basis of the input preparation for L3-5 was an existing file which had previously been used for RELAP5/MOD2 fast transient calculations on LOFT. It was necessary to update and expand the input file, and several of the available input listings (7, 8, 9) were used. The reasons for particular approaches used in modelling are presented below. Figure 2 shows the nodalization used. The input listing is given in Appendix A.

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3.2.1 The Initial System Pressure

To avoid an explicit steady-state pressurizer pressure and level control, the surge line junction was modelled as a trip valve which was closed until scram. The pressurizer initial fluid conditions were saturated with correct fluid content and pressure. In the case A calculation no boundary heat structures were involved in keeping the pressurizer state steady. However, for cases B and C pressurizer heat structures were applied with the outer surface at saturation temperature until scram and thereafter at room temperature.

A time dependent volume was connected to the pressurizer surge line by a trip valve adjacent to the pressurizer bottom in order to maintain the initial primary pressure constant during the steady state calculation. During steady state the pressurizer was isolated from the surge line. The pressure of the time dependent volume was equal to the pressure in the bottom volume of the pressurizer. At scram time the trip valve closed and the pressurizer isolation ceased.

3.2.2 Primary Fluid Temperatures

The bulk heat loss occurred in the steam generator. Effects from structural heat losses, pump power and pump cooling water were relatively small. The base case fluid temperatures in the hot leg were 576 ± 2 K and in the cold leg 558 ± 1 K (5). These temperatures satisfy the loop flow heat balance.

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It was observed that some of the primary fluid temperature measurements were not consistent with the heat balance. For example, the core inlet temperature (TE-ILP-001 in the experiment) was 3 K higher than the cold leg fluid temperature. Several upper plenum thermocouple measurements showed temperatures which were as much as 10 K higher than the measured hot leg fluid temperature. The reason for these inconsistencies can not be fully understood although three-dimensional flow might be the main cause. Furthermore, the steam generator inlet to outlet temperature difference was about 4 K lower than it ought to be. The measured temperatures had mostly uncertainties of about 3 K or more (5).

3.2.3 Core Flow Bypass

Several core bypass flow paths existed. The following two (7) were modelled by series valves in order to adjust the flows before scram:

- The inlet annulus to upper plenum with 6.6 % of the primary loop flow
- The lower plenum to upper plenum with 3.6 % of the primary loop flow.

The reflood assist bypass valve leakage and the broken loop heat up lines were not explicitly modelled since the mass flow rates were quite small. The reflood assist bypass valve leakage is further discussed for the case C calculation (see 5.2 below).

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3.2.4 Environmental Heat Losses

The exchange of heat with structural material is important in small break analysis. Since the available input had only restricted material included, structures had to be added to the input. The bulk structures of the facilities were modelled to represent the correct structural masses.

For RELAP5/MOD2 an overall environmental heat transfer coefficient was determined by test calculations in order to obtain approximately the total heat loss of 250 kW as found in the experiment (7).

3.2.5 Break Discharge Coefficient

Test calculations showed a too rapid decrease in pressurizer fluid inventory when the default subcooled discharge coefficient of unity was used. Using a coefficient of .85 the rates of emptying the pressurizer and of the early system depressurization were close to the experiment. The assumption that the pressurizer emptying rate is an indicator of the break discharge flow is only applicable for low pressure drop in the surge line as it occurs in small break experiments.

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3.2.6 Pump Model

The primary coolant pumps were tripped .8 s after the break. Coast down followed under the influence of the coolant flow inertia and the pump moment of inertia. Since the primary pumps in the experiment have a too small moment of inertia, compared to that of commercial PWRs, their coastdown was simulated by a fluid clutch coupling to a motor-generator driving unit. When the speed reached 12.5 Hz (10) the coupling was disconnected.

The combined inertia of the pump and the motor-generator flywheel was modelled by pump inertia data closely similar to those reported by T R White (11). The inertia polynomial was modified to avoid negative moment of inertia at higher pump speeds.

3.2.7 Steam Generator

The steam generator steady state was achieved using auxiliary components. The pressure was maintained by a steam filled control volume connected to the steam generator top. The downcomer level was attained through a flow controlled junction connecting a time dependent volume to the upper part of the downcomer.

The main steam valve was modelled as a time dependent junction rather than a motor or servo valve. The main reason for this was to use the steam flow (6) directly as boundary value and also to facilitate modelling of the pressure dependent leakage of the closed valve (7).

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Closure of the steam valve started from the experimental initial flow at 5.58 MPa (steam generator pressure and a 2.0 MPa downstream pressure. After the valve closure had been initiated a secondary pressure of 6.9 MPa was assumed in order to obtain the mass flow from the curve giving the valve characteristic as a function of stem lift (6). The leakage from the closed valve which was .053 kg/s at 4.19 MPa (7), was assumed to be proportional to the secondary pressure measured in the experiment.

The feedwater valve was modelled as a time dependent junction which gave the experimental mass flow until closure of the valve. The feedwater valve closure was assumed to be as fast as in the LOFT base input. Test calculations showed that the predicted secondary pressure continued to increase more than in the experiment when the steam valve began to close. Discrepancies in the downcomer level and the pressure behaviour could be suspected to be caused by the fast feedwater valve closure. An example of a different valve closure rate is given in a calculation for the L3-6 experiment carried out by L N Kmetyk (9) who used a rate of 5 %/s similar to the rate of the main steam valve.

No feedwater temperature data were found in available reports. Therefore the steam generator operation was achieved by controlling the feedwater internal energy so that the sum of steam generated in each secondary volume was equal to the main steam valve mass flow. This procedure achieves a steam generator steady state irrespective of the tube package heat transfer, or the heat exchange with structures.

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4 THE BASE CASE CALCULATION (CASE A)

The input listing of case A is given in Appendix A.

After the depressurization had reached saturation conditions obstinate fluctuations in the calculation time step were observed. This effect was arrested by reducing the maximum time step from 1. s to .4 s. From previous experience, the RELAP5/MOD2 time step control may reduce the time step so much, after preceeding long time steps, that even execution error might occur.

Mid-transient water packing occurred several times due to water plugs in the cold leg passing forth and back at the break line T-junction. The code water packing mitigation scheme dealt correctly with the calculated pressure spikes, and as a result the calculation could be continued.

The results of the comparisions are shown in Appendix B. Primary system pressures are shown in Plots B.21, B.22, B.27, B.34, B.35 and B.43. After the subcooled depressurization, the primary system pressure is underpredicted until about 900 s. It is noted that the experiment depressurizes at an increased rate in the time interval from about 600 s to 1200 s which is not reflected in the calculations. The primary fluid temperatures, Plots B.9, B.17, B.18, B.20, B.26, B.33, B.41 and B.44, show the corresponding discrepancies. The pressure and temperature comparisons at the secondary side, Plots B.51 and B.50 respectively, are also similar. The

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decreased depressurization rate after about 1000 s is caused by the increased temperature difference between primary and secondary sides shown in the experiment, but not in the calculations, Plot B.52.

A contributory cause for the mid-transient increase of the experimental depressurization rate is the hot leg steam production, Plots B.23 and B.24, which occurs in the time interval from 450 s to 800 s. The case A shows a corresponding density decrease but it is delayed by about 500 s, and the calculated water content is not reduced to the low experimental level.

The cold leg densities, Plots B.28 and B.30, show opposite differences - the calculated densities are lower than the experimental densities.

The predicted main recirculation flows, Plots B.11, B.25 and B.39, cannot be assessed due to unqualified experimental data (5). The experimental hot leg mass flow, Plot B.25, is qualified for the initial condition only. Condie et al (7), assume that natural circulation continued in the experiment from pump coast down until 750 s.

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5 SENSITIVITY CALCULATIONS

The case A comparisons, discussed in Chapter 4, revealed some discrepancies which were studied by two sensitivity calculations, case B and case C. The salient problems concern the fast early phase of the depressurization and the primary fluid temperatures.

5.1 Case B

The input changes introduced to the case B calculation were aimed at improving the predictions early in the transient until 250 s. Two updates were introduced in the steam generator modelling in this sensitivity study.

The first update was to change the main steam valve leakage after 68 s. Due to instrument noise the main steam valve started to open at about this time and operated intermittently during a period of 10 s. The unintended valve cycle is evident from the secondary pressure, Plot B.51. The base case calculation had used the valve threshold mass flow, see valve characteristic (6), which at the prevailing pressure, ought to have been about 5.7 kg/s. However, the pressure comparison, Plot B.51, shows a predicted pressure drop rate starting at 68 s which is about twice that of the experiment. Consequently, the steam mass flow in the case B was halved during the main steam valve open cycle, and a pressure drop rate close to the measured one was calculated.

The second update concerned the downcomer liquid level which had shown discrepancies, Plot B.49. Even though a questionably slow closure of

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the feed water valve was applied in case A the liquid level was predicted not to start to recover by the auxiliary feed, until about 400 s as compared to about 100 s in the experiment. A contribution to that discrepancy would follow from a predicted excess steam production in the lower part of the riser section. A check-up of the steam generator tube section primary and secondary volumes distribution revealed an inconsistency in the initial, case A, base input used. Due to this error much steam was generated in the lower riser volumes. A more correct tube structure distribution was introduced. However, only a slightly better agreement with the experimental level rise turned out.

Some water still remained distributed in the pressurizer after the emptying period, Plot B.54. The reason had been an unjustified application of the junction equal phase velocity between the uppermost pressurizer volumes. A correction was applied even though no apparent effect on the prediction plots would be expected.

5.2 Case C

The next calculation, case C, focused on the primary side hydraulic scenario. The loop mass flow rate was not measured during the transient. Moreover, the vessel downcomer and upper plenum water contents measured by conductivity probes, and presented as bubble plots (5), suffered from error margins when converted into level heights, Plots B.15 and B.16.

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After disconnection of the flywheels the low internal moment of inertia of the two recirculation pumps will make the speed of the two recirculation pumps sensitive to the loop mass flow. Plot B.37 evidently shows that the intact loop flow of the experiment ceases at about 130 s. The cases A and B show a prolonged and gradual flow decrease. These two calculations had about 20 kg/s primary mass flow at 250 s through the steam generator. A reverse flow of about 6 kg/s prevailed in the vessel inlet annulus to the outlet plenum junction. There was also a 1.5 kg/s reverse core bypass flow. Thus three paths of natural circulation due to the core decay heat have been identified.

The modeled flow bypass from the vessel inlet annulus to the upper plenum was insufficient to reduce the intact loop driving pressure difference to stop the main fluid flow in the previous predictions as early as in the experiment. This may have partly been caused by the omission of the reflood assist bypass valve (RABV) in the model. The reason for the omission was that the initial RABV vessel bypass flow was quite low and uncertain. Likewise the broken loop hot leg and cold leg fluid temperatures did not indicate any substantial initial RABV leakage.

The previous discussion focused on the natural circulation in the intact loop due to the core decay heat. A flow reduction could result from an increased bypass flow area between the inlet annulus and the upper plenum. It was intended, for the case C calculation, to determine an area which terminates the loop

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circulation at about the same time as in the experiment. To obtain the initial intact loop mass flow a servo valve was used as the junction between the inlet annulus (vol.290) and the downcomer (vol.205). Valve control was applied only through the steady state. Ideally, the flow control ought to have been applied at the inlet nozzle (junction between vols. 185 and 290). A cross junction modelling, however, cannot be applied for a valve component.

The leakage from the cold leg inlet annulus to the upper plenum is caused by a flow path in the narrow gap between the vessel filler blocks and the vessel wall. This leakage path has a vertical extension equal to the nozzle diameter. To enhance a reduction of the transient pressure difference over the core, the leakage junction was divided into two junctions at slightly different elevations. One leakage path connected the upper ends of the adjacent volumes below the inlet and the outlet annuli. The other path similarly connects the bottom ends of the volumes above the inlet and the outlet annuli. This higher level leakage will, compared to the previous modelling, promote steam bypass, and thus contribute to a lower pressure difference between vessel outlet and inlet .

The split up of the core bypass into two different leakage paths did not reproduce the fast pump coast down at 130 s as seen in Plot B. 37. However, some improvement was obtained as can be seen from the data uncertainty analysis in Appendix C (experiment code CLAX). In addition the core clad temperatures, Plots B.3 through B.6, obtained in the case C are more similar to the experiment than the two previous cases. This

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is more evident from Figure 3 which compares the time derivatives, obtained from Plot B.5, of the predicted and experimental clad temperatures. Evidently, the model change in the flow bypass had a positive impact on the core fluid distribution. Moreover, the case C break fluid density dropped at the same time as in the experiment (at about 130 s). see Plot B.38.

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6 RUN STATISTICS

The input model for the base case RELAP5/MC52 calculation for LOFT L3-5 encompassed:

113	volumes
120	junctions
99	heat structures

The volumes include two pump components, one separator component and nine time dependent volumes of which three were used for the steady state. Among the junctions there are totally five valve components and four time dependent junctions which are connected during steady state.

During the transient calculation the following resources were used:

Computer time	CPU=25778 s
Number of time steps	DT =12374
Number of volumes	C =113
Transient real time	RT =2032 s

resulting in the following code efficiency factor (1)

$$\frac{\text{CPU} * 10^3}{C * \text{DT}} = 18.44$$

The computer used was a Cyber 170-810.

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7 CONCLUSIONS

The LOFT small break experiment L3-5 has been assessed using the RELAP5/MOD2 code. Three calculations were carried out; one base case calculation and two sensitivity calculations with model changes concerning the steam generator operation and the core bypass mass flow. The transient predictions compare reasonably well with the experiment as regards first-hand parameters such as system pressures and fluid temperatures. Uncertainties, over time intervals, of the predicted data compared with the experiment are given in Appendix C.

In the calculated steady state, the experimental initial data could be fairly well reproduced. Some experimental fluid temperatures, particularly in the upper part of the vessel, revealed relatively large discrepancies which could not readily be explained.

The predicted start of voiding in the intact loop hot leg as well as the cold leg occurred late as compared to the experiment although the predicted system pressure was underestimated.

The steam generator liquid level rise, recovered by the auxiliary water feed, was underpredicted in case A. Although the limited steam generator experimental data available do not help to single out any particular detail in the model as the cause, the most probable reason is the underestimation of the water content early in the test.

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In the case B calculation, the steam generator boiling region was remodelled to promote void formation at higher elevations. The improvement gained in the transient downcomer level was rather limited. A contributory cause for the discrepancy in the level could be a significant droplet field initially residing in the space between the primary separator, modelled by the RELAP5 separator component, and the mist extractor adjacent to the steam line nozzle. Imposing a predetermined steady state water content on this space is, however, not possible unless the geometric model is considerably modified.

The case C calculation concentrated on the primary mass flow rate. The downcomer to upper plenum leakage was split into one junction promoting the steam bypass and an other one the water bypass in the case of voided fluid in the cold leg. The clad temperatures as well as the break fluid density were improved.

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Table 1

Initial conditions

Quantity		Measured	Predicted		
			Case A	Case B	Case C
Primary coolant system					
Mass flow rate	(kg/s)	476.4	478.8	476.4	476.6
Hot leg pressure	(MPa)	14.86	14.86	14.87	14.86
Cold leg temperature	(K)	558.	557.4	559.4	559.9
Hot leg temperature	(K)	576.	576.4	578.4	579.6
Reactor vessel					
Power level	(MW)	49.	49.0	49.	49.
Pressurizer					
Water temperature	(K)	614.6	614.7	614.7	614.7
Pressure	(MPa)	14.88	14.88	14.88	14.88
Liquid level	(m)	1.25	1.25	1.25	1.25
Broken loop					
Cold leg temperature	(K)	556.	555.	555.	554.
Hot leg temperature	(K)	562.	561.	561.	559.
SG secondary side					
Water level	(m)	0.19	0.19	0.19	0.19
Water temperature	(K)	543.	544.	534.	532.
Pressure	(MPa)	5.58	5.50	5.58	5.58
Mass flow rate	(kg/s)	26.4	26.2	26.0	26.0

Table 2

Sequence of events

Event	Imposed action	System reaction	Time (s)		
			Case A	Predicted Case B	Case C
Reactor scrammed	-4.8		-4.8	-4.8	-4.8
LOCA initiated	0.		0.	0.	0.
Primary coolant pumps tripped		0.8	0.9	0.9	0.9
HPIS injection initiated (13.2 MPa)		4.0	2.5	2.6	3.3
Primary pump coastdown complete (12.5 Hz)		17.7	20.8	17.9	20.3
Pressurizer emptied		22.2	24.4	23.6	24.4
Upper plenum reached saturation		28.4	38.3	37.3	35.7
Intact loop hot leg voiding begin		30.	42.	45.	45.
SCS auxiliary feed initiated	63.		63.	63.	63.
Intact loop cold leg voiding begin		80.	138.	133.	147.
End of subcooled break flow		92.9	140.	109.	163.
SCS pressure exceeds primary pressure		745.	1810.	1490.	not obtnd.
Primary fluid mass at minimum		1480.	not obtnd.	1750.	not obtnd.
SCS auxiliary feed terminated	1800.		1800.	1800.	1800.

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Table 3

Parameters plotted and used in the assessment comparisons.

COMPONENT	CONTINUOUS PARAMETER #	EXPERIMENT (IDENTIFIER)	PREDICTION (MINOR EDIT)	PLOT IDENTIF. EXP.	PLOT IDENTIF. CALC.	PLOT NO.	
CORE	FLUID DENSITY (INLET)	**	CNTRLVAR 901	C 17		B. 1	
	HEATING POWER	**	RKTPW 0	C 27		B. 2	
	CLAD TEMPERATURE, VOLUME 1 (BOTTOM)	TE-2014-011 TE-506-011 TE-516-005	CNTRLVAR 903	C 3X	C 37	B. 3	
	- * - , VOLUME 2	TE-1F7-016 TE-1F7-021 TE-2008-021 TE-4114-021 TE-514-016 TE-516-021	CNTRLVAR 903	C 4X	C 47	B. 4	
	- * - , VOLUME 3	TE-1F7-026 TE-1F7-030 TE-2014-030 TE-2H01-032 TE-4H14-028 TE-4H14-032 TE-5H7-026	CNTRLVAR 905	C 5X	C 57	B. 5	
	- * - , VOLUME 4	TE-2006-039 TE-2H01-037 TE-3011-039 TE-4114-039 TE-5H6-037	CNTRLVAR 906	C 6X	C 67	B. 6	
	- * - , VOLUME 5	TE-2014-045 TE-4014-045 TE-5F9-045 TE-506-045 TE-5H5-049	CNTRLVAR 907	C 7X	C 77	B. 7	
	- * - , VOLUME 6 (TOP)	TE-5H7-058 TE-506-062	CNTRLVAR 908	C 8X	C 87	B. 8	
	TEMPERATURE (OUTLET)	TE-1UP-001 TE-5UP-001 TE-5UP-003	CNTRLVAR 905	C 9X	C 97	B. 9	
	TEMP. DIFF. (OUTLET-INLET)	TE-1UP-001 TE-1LP-001	CNTRLVAR 910	C AX	C A7	B. 10	
	CORE FLOW (INLET)	**	MFLOWJ 125.01		C 87	B. 11	
	CORE INVENTORY	POE-RV-002	**	CNTRLVAR 912	C 07	B. 12	
	VESSEL	DOWNCOMER MASS INVENTORY	POE-RV-003	**	CNTRLVAR 913	V 17	B. 13
		MASS INVENTORY (TOTAL VESSEL)	**	CNTRLVAR 914	V 27		B. 14
		DOWNCOMER LIQUID LEVEL	LE-15T-001	***	CNTRLVAR 915	V 3X	V 37
UPPER PLENUM LIQUID LEVEL		LE-3UP-001	***	CNTRLVAR 916	V 4X	V 47	B. 16
DOWNCOMER TEMPERATURE (INLET)		TE-15T-001 TE-25T-001	TEMPF 205	V 5X	V 57	B. 17	
UPPER PLENUM TEMPERATURE		TE-1UP-001 TE-4UP-001 TE-5UP-001	TEMPF 240	V 6X	V 67	B. 18	
UPPER PLENUM FLUID SUBCOOLING		SC-5UP-102 ST-1UP-111 TE-1UP-001	CNTRLVAR 919	V 7X	V 77	B. 19	
LOWER PLENUM TEMPERATURE		TE-1LP-001	TEMPF 225	V 8X	V 87	B. 20	
UPPER PLENUM PRESSURE		PE-1UP-001A1	P 245	V 9X	V 97	B. 21	
LOWER PLENUM PRESSURE		PE-15T-001A PE-25T-001A	P 225	V AX	V A7	B. 22	
HOT LEG	FLUID DENSITY (I.L.)	DE-PC-205 DE-PC-002A DE-PC-002B DE-PC-002C	**	RHO 105	HL1X	HL17	B. 23
	FLUID DENSITY (B.L.)	DE-BL-002B	**	RHO 305	HL2X	HL27	B. 24
	MASS FLOW RATE	FT-P139-27-1 FT-P139-27-2 FT-P139-27-3	** ** **	MFLOWJ 110		HL37	B. 25
	TEMPERATURE (I.L.)	TE-PC-002B	**	TEMPF 105	HL4X	HL47	B. 26
	PRESSURE (I.L.)	PE-PC-002	**	P 105	HL5X	HL57	B. 27

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COLD LEG	FLUID DENSITY (I.L.)	DE-PC-118 DE-PC-001A DE-PC-001B DE-PC-001C	**	RHO 180	CL1X	CL1Y	B 28
	FLUID DENSITY (I.L. PUMP SUCTION)	DE-PC-305 /DE-PC-003A/ /DE-PC-003B/ /DE-PC-003C/	**	RHO 115.13	CL2X	CL2Y	B 29
	FLUID DENSITY (B.L.)	DE-BL-105 DE-BL-001A DE-BL-001B DE-BL-001C	**	RHO 345	CL3X	CL3Y	B 30
	LIQUID LEVEL (I.L. LOOP SEAL)	LEPDE-PC-020		CNTRLVAR 931	CL4X	CL4Y	B 31
	- " - (B.L.)	LEPDE-BL-014	**	CNTRLVAR 932		CL5Y	B 32
	TEMPERATURE (I.L. NEAR VESSEL)	TS-PC-004		TEMPF 185	CL6X	CL6Y	B 33
	PRESSURE (I.L.)	PE-PC-005		P 120	CL7X	CL7Y	B 34
	- " - (B.L.)	PE-BL-001		P 345	CL8X	CL8Y	B 35
	PRESS. DIFF. (ACROSS THE PUMPS)	PDE-PC-001		CNTRLVAR 935	CL9X	CL9Y	B 36
	PUMP SPEED (PUMP 1)	RPE-PC-001		PMPVEL 135	CLAX	CLAY	B 37
BREAK	FLUID DENSITY	DE-PC-S02A		RHO 800	BR1X	BR1Y	B 38
	MASS FLOW RATE	FR-PC-SBRK		MFLOWJ 805	BR2X	BR2Y	B 39
	ENERGY RELEASE	**		CNTRLVAR 940		BR3Y	B 40
	INLET TEMPERATURE	TE-PC-S01C		TEMPF 800	BR4X	BR4Y	B 41
	INLET SUBCOOLING	ST-PC-S101 TE-PC-S01C		CNTRLVAR 942	BR5X	BR5Y	B 42
	INLET PRESSURE	PE-PC-S01		P 800	BR6X	BR6Y	B 43
	SG PRI. SIDE	TEMPERATURE (INLET)	TE-SG-001		TEMPF 115.03	SP1X	SP1Y
TEMP. DIFF. (INLET-OUTLET)		TE-SG-001 TE-SG-002		CNTRLVAR 945	SP2X	SP2Y	B 45
PRESSURE DIFF.		POE-PC-002		CNTRLVAR 946	SP3X	SP3Y	B 46
SG SEC. SIDE	FLUID DENSITY	**		RHO 515.03		SS1Y	B 47
	MASS FLOW RATE	**		MFLOWJ 516		SS2Y	B 48
	LIQUID LEVEL	LD-P004-008B		CNTRLVAR 949	SS3X	SS3Y	B 49
	LIQUID TEMPERATURE	TE-SG-003		TEMPF 515.03	SS4X	SS4Y	B 50
	PRESSURE	PE-SG5-001		P 530.01	SS5X	SS5Y	B 51
SG	PRIMARY-SECONDARY TEMP.-DIFF. (AT INLET)	TE-SG-001 TE-SG-003		CNTRLVAR 952	S 1X	S 1Y	B 52
	HEAT TRANSFER RATE	**		CNTRLVAR 953		S 2Y	B 53
PRESSURIZER	LIQUID LEVEL	LT-P138-006		CNTRLVAR 954	P 1X	P 1Y	B 54
	LIQUID TEMPERATURE	TE-P138-020		TEMPF 415.02	P 2X	P 2Y	B 55
	STEAM TEMPERATURE	TE-P138-019		TEMPG 415.07	P 3X	P 3Y	B 56
	PRESSURE	PE-PC-004		P 415.08	P 4X	P 4Y	B 57
ECCS	HPIS VOLUMETRIC FLOW RATE	FI-P128-104		CNTRLVAR 958	EC1X	EC1Y	B 58
SYSTEM	MASS BALANCE (INTEG. FROM BREAK NO PUMP SEAL W.)	**		CNTRLVAR 959		SY1Y	B 59
	COOLANT EGY. BALANCE (INTEGR.)	**		CNTRLVAR 960		SY2Y	B 60
	PRIM. EXTERNALS HEATFLOW	**		CNTRLVAR 962		SY3Y	J. 2
RELAPS	COMPUTATION CPU TIME	**		CPUTIME 0		R 1Y	B 61
	COMPUTATION MASS ERROR	**		EMASS 0		R 2Y	B 62

* THE COMPARISON PARAMETERS ARE THOSE REPORTED AS DIRECTLY MEASURED OR AS COMPUTED RESULTS FROM THE EXPERIMENT

** NO DATA AVAILABLE FROM THE EXPERIMENT

*** DATA OBTAINED FROM BUDDLE PLOT IN EXPERIMENT REPORT

/ / EXPERIMENT DATA AVAILABLE BUT NOT USED IN COMPARISONS

? CALCULATION CASE (A, B OR C)

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Table 4

Measurement errors

Quality	Uncertainty	Comment
Pressure	251-282 kPa 120 kPa	Primary side Secondary side
Fluid temp	2.7-3.1 K .5 K 5.9 K 10.4 K	Mostly TE-P139-019, steam TE-SG-001, TE-SG-002 TE-PC-004
Fluid density	78-82 kg/m ³ 129-131 kg/m ³	Mostly DE-BL-001A, DE-BL-001C DE-PC-002B, DE-PC-002C
Clad temp	3.1-3.2 K	All
Diff pressure	.49 k Pa 1. kPa 1.3 kPa 1.8 kPa	PDE-RV-003 PDE-PC-002 PDE-RV-002 PDE-PC-001
Mass flow	.02 L/s 6.3 kg/s 17 kg/s 25 percent 1 kg/s	HPIS I.L. init condition I.L. hot leg Break, 40-750 s Break, 750-2100 s
Liq level	.04 m .05 m .099-.137 m Bubble plot	Pressurizer SG secondary Cold legs Upper plen, downcomer
Speed	1.22 rad/s	Main recirc pumps

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Table 5

RELAP5/MOD2 code features.

COMPUTATION PROCESSING FEATURES

- Several problem type and execution control options as
 - a. steady state initialisation using fictitious structure heat capacities for faster convergence
 - b. transient calculation
 - c. strip type execution, to select requested parameters from a restart file
 - d. trip system, to decide on actions during calculation due to reaching specified conditions in calculation parameters.
 - e. ability to delete or add hydrodynamic components, structure components and control variables at a restart of calculation.

CLASSIFICATION OF HYDRODYNAMIC MODEL

- One-dimensional, with provisions for
 - a. choked flow model
 - b. abrupt area change model
 - c. cross flow junctions.
- Two-fluid, six equation, space-time numerical solution scheme.
- flow regime oriented field characteristics depending on mass flux and void fraction for
 - a. horizontal flow with bubbly, slug, mist and stratified fields
 - b. vertical flow with bubbly, slug, annular-mist (and stratified) fields
 - c. high mixing flow with bubbly and mist fields (for pumps).

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Table 5 cont'dHYDRODYNAMIC COMPONENTS (Input systematics)

- Volume type components
 - a. single volume
 - b. pipe and annulus, for condensed input of several similar single volumes
 - c. time dependent volume, for defining a boundary source with a time dependent fluid state
 - d. branch, a volume capable of two or more connecting junctions at either end
 - e. pump, characterized by rated values for flow, head, torque, density and moment of inertia. The single phase homologous curve, two-phase multipliers and phase difference tables to model the dynamic pump behaviour
 - f. special system components for steam separator, jetmixer, turbine and accumulator.
- Junction type components
 - a. single junction
 - b. time dependent junction, for a time dependent junction flow with a time dependent or controlled flow state
 - c. cross-flow junction, to model a small cross flow, a tee branch or a small leak flow
 - d. valve, various operation characteristics available for check valve, trip valve, inertial valve and relief valve.

INTERPHASE CONSTITUTIVE EQUATIONS

- Interphase drag
 - a. steady drag due to viscous shear depending on flow regime. Semi-empirical mechanisms to describe flow regime transitions
 - b. dynamic drag due to virtual mass effect.
- Interphase mass and heat transfer depending on flow regime and the fluid fields to saturation temperature differences

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Table 5 cont'dFLUID TO WALL CONSTITUTIVE EQUATIONS

- Wall friction due to wall shear effects formulated for flow regimes and based on a two-phase multiplier approach.
- Wall heat transfer depending on flow characteristics defined for
 - a. single-phase forced convection (Dittus-Boelter)
 - b. saturated nucleate boiling (Chen)
 - c. subcooled nucleate boiling (modified Chen)
 - d. critical heat flux (Biasi or modified Zuber)
 - e. transition film boiling (Chen)
 - f. film boiling (Bromley-Pomeranz and Dougall-Rohsenow)
 - g. condensation (partly Dittus-Boelter).
- Interfacial mass transfer at the wall depending on wall, fluid and saturation temperatures for
 - a. subcooled and saturated boiling
 - b. transition film and film boiling
 - c. condensation.

HEAT STRUCTURES

These may be rectangular, cylindrical or spherical in shape. The structure position is defined through component numbers of left and right hand side hydraulic components. A structure is physically defined by the geometry and the temperature dependent conductivity and volumetric heat capacity data. The structure model is further specified by the number of internal mesh points in the direction of heat flow.

CONTROL COMPONENTS

By these new (control) variables are defined from calculated parameters using algebra, standard functions, trip type operands or integrals.

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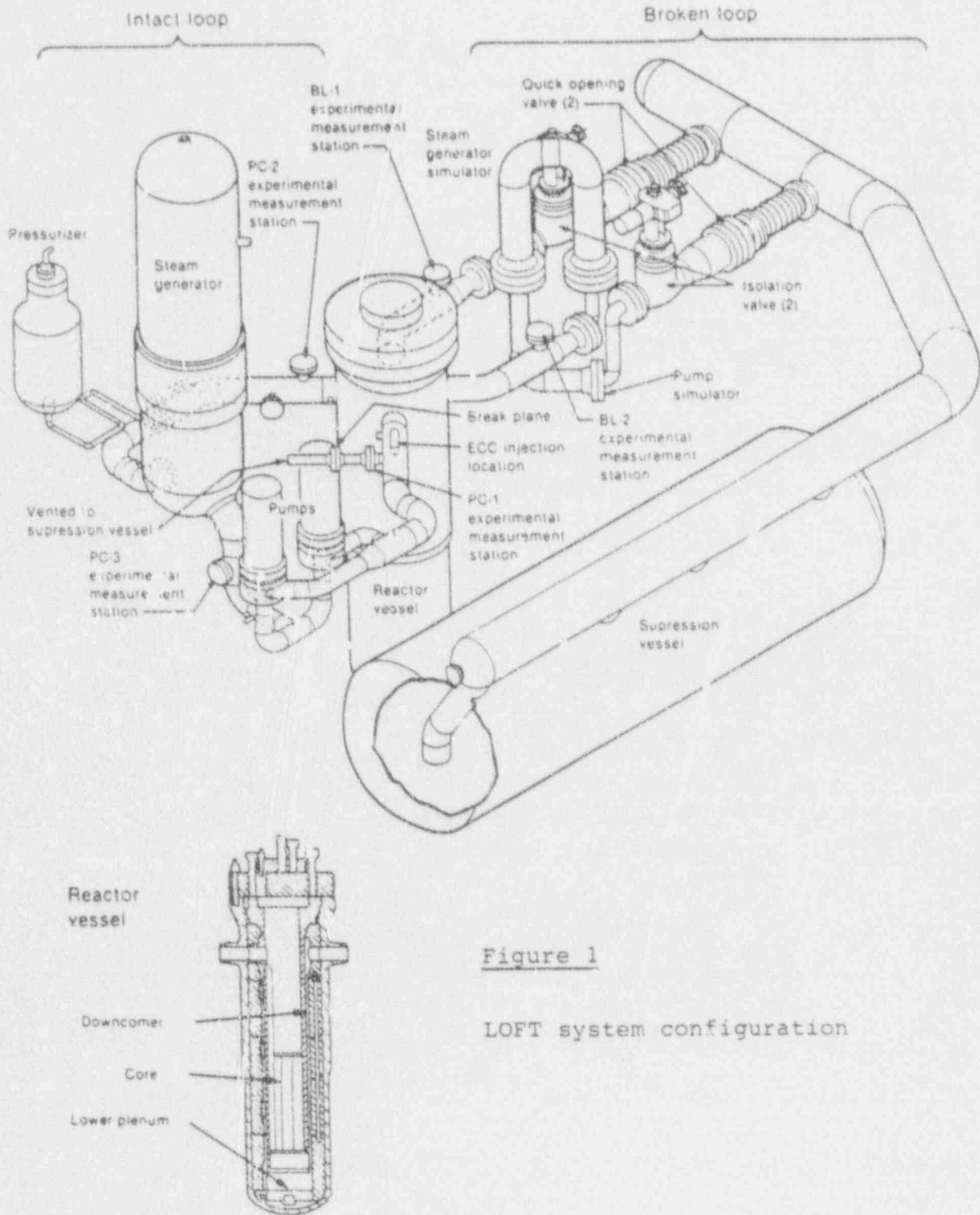


Figure 1

LOFT system configuration

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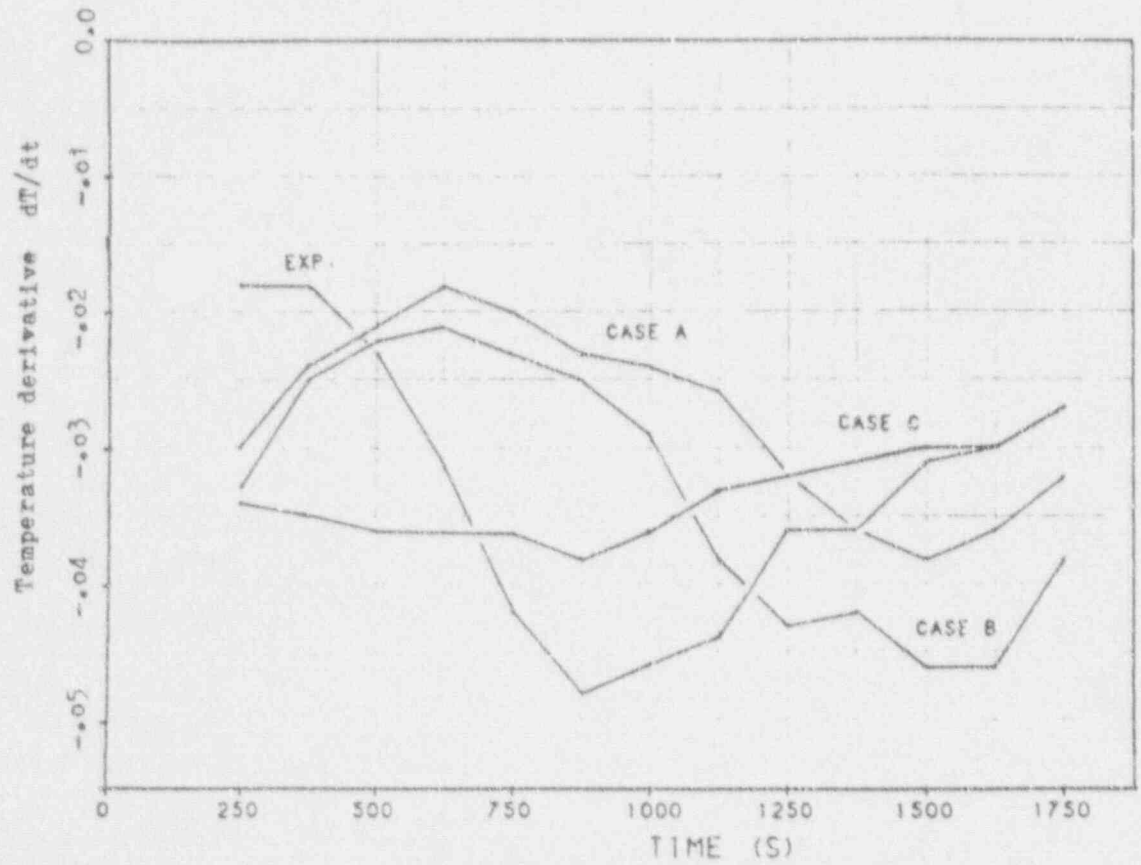


Figure 3 Time derivative of the core volume 3 clad temperature

Input listing (Case A)

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* ** LOFT L3-5 ANALYSIS (PRIMARY+SECONDARY+KINETICS) **

*
0000100 RFW STDY-47
*
0000101 RUN
*
0000102 SI SI
*
*0000104 HOACTION
*
0000105 40. 60.0
*
0000120 100010000 0 0 WATER PRIMARY
0000121 517010000 0 0 WATER SECONDARY
*
* TIME END MIN STP MAX STP SDY OPT KOR MAJR RST *
0000200 45.3 1.0E-5 4 00001 5 200 200

* MINOR EDIT VARIABLES FOR THE ICAP ASSESSMENT

* CORE

0000301 CNTRLVAR 901
0000302 RKTPOW 0
0000303 CNTRLVAR 903
0000304 CNTRLVAR 904
0000305 CNTRLVAR 905
0000306 CNTRLVAR 906
0000307 CNTRLVAR 907
0000308 CNTRLVAR 908
0000309 CNTRLVAR 909
0000310 CNTRLVAR 910
0000311 MFLOWJ 225010000
0000312 CNTRLVAR 912

* VESSEL

0000313 CNTRLVAR 913
0000314 CNTRLVAR 914
0000315 CNTRLVAR 915
0000316 CNTRLVAR 916
0000317 TEMPF 205010000
0000318 TEMPF 240010000
0000319 CNTRLVAR 919
0000320 TEMPF 225010000
0000321 P 245010000
0000322 P 225010000

* HOT LEG

0000323 RHO 105010000
0000324 RHO 205010000
0000325 MFLOWJ 1 2010000
0000326 TEMPF 105010000
0000327 P 105010000

* COLD LEG

0000328 RHO 185010000

0000329 RHO 115020000
0000330 RHO 245010000
0000331 CNTRLVAR 931
0000332 CNTRLVAR 932
0000333 TEMPF 185010000
0000334 P 120010000
0000335 P 345010000
0000336 CNTRLVAR 936
0000337 MPPVEL 135

* BREAK

0000338 RHO 185010000
0000339 MFLOWJ 205000000
0000340 CNTRLVAR 940
0000341 TEMPF 800010000
0000342 CNTRLVAR 942
0000343 P 185010000
0000344 TEMPF 115030000

* STEAM GENERATOR

0000345 CNTRLVAR 945
0000346 CNTRLVAR 946
0000347 RHO 515030000
0000348 MFLOWJ 515000000
0000349 CNTRLVAR 949
0000350 TEMPF 515030000
0000351 P 530010000
0000352 CNTRLVAR 952
0000353 CNTRLVAR 953

* PRESSURIZER

0000354 CNTRLVAR 954
0000355 TEMPF 415020000
0000356 TEMPF 415020000
0000357 P 415080000

* ECCS

0000358 CNTRLVAR 958

* SYSTEM

0000359 CNTRLVAR 959
0000360 CNTRLVAR 960
0000362 CNTRLVAR 962

* RELAPS

0000361 CPU TIME 0
0000362 EMASS 0

* TRIP INPUT DATA

* 501 SCRAM REACTIVITY DER TABLE 609
* MAIN STEAM VALVE CLOSE 550
* FEED WATER VALVE CLOSE 580
*
* 510 S OAK TIME AUX FEED WATER 548
*

* 511 TRIP PUMP 1 125
PUMP 2 163
*
* 516 BREAK CLOSE 805
*
* 515 AFTER EXPERIMENT END
*
* 518 MFLOW DIRECTION OF FLOW FROM COPE 240
*
* 525 SO S EXP. BREAK FLOW QUALIFIED 805
*
* 500 STOP ADV. OF CALCULATION
*
* 545 BREAK OPEN 805
*
* 545 PRESS. VALVE OPEN. AFTER SS 435
*
* 581 MOPIS INITIATED 640
*
* 599 PUMP COOLANT INJECTION 901
*

* 501 TIME 0 GE NULL 0 45.2 L
* 502 TIME 0 GE NULL 0 0.0 L
* 510 TIME 0 GE TIMEOF 501 4.8 L
* 511 TIME 0 GE TIMEOF 510 .8 L
* 512 TIME 0 GE NULL 0 13.3E8 L
* 513 P 100010000 LE NULL 0 2.15E6 L
* 514 P 100010000 LE NULL 0 2.15E6 L
* 515 TIME 0 GE TIMEOF 514 20. L
* 516 VELFJ 240010000 GE NULL 0 0.0 L
* 520 P 530020000 GT NULL 0 5.63E6 L
* 521 P 530020000 LT NULL 0 5.61E6 L
* 522 P 530020000 GT NULL 0 5.55E6 L
* 523 P 530020000 LT NULL 0 5.53E6 L
* 530 CNTRLVAR 10 LT NULL 0 3.10 L
* 531 CNTRLVAR 10 GT NULL 0 3.18 L
* 535 TIME 0 GE TIMEOF 510 50. L
* 536 TIME 0 GT TIMEOF 510 83. L
* 561 P 100010000 GT P 530020000 0. L
* 562 TIME 0 GE TIMEOF 660 1800. L
*
* 514 AND 581 N
* 513 AND -514 N
* 599 AND -514 N
* 501 OR 602 N
* 502 AND 601 N
* 503 AND 602 N
*
* 512 OR 620 N
* 511 AND -615 N
* 512 AND 610 N
*
* 512 OR 523 N
* 514 AND -522 N
* 515 AND 501 N
* 516 AND -614 N
*
* 533 AND -660 N
* 534 OR 603 N
* 534 AND 510 L
*
* 545 AND -514 N

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1352500 7 7
 1352501 -1.000000E+00 -1.000000E+00
 1352502 -3.000000E-01 -3.000000E-01
 1352503 -1.000000E-01 -5.000000E-01
 1352504 0.000000E+00 -4.500000E-01

 * FOR TORQUE CURVE NO. 8
 *

1352600 7 8
 1352601 -1.000000E+00 -1.000000E+00
 1352602 -7.500000E-01 -9.000000E-01
 1352603 -3.000000E-02 -8.000000E-01
 1352604 0.000000E+00 -8.700000E-01

 * TWO - PHASE MULTIPLIER DATA
 *

 * HEAD CURVE
 *

1353000 0 0
 1353001 0.000000E+00 0.000000E+00
 1353002 2.000000E-02 2.000000E-02
 1353003 6.000000E-02 5.000000E-02
 1353004 1.000000E-01 1.000000E-01
 1353005 2.000000E-01 4.500000E-01
 1353006 2.400000E-01 8.000000E-01
 1353007 3.300000E-01 9.000000E-01
 1353008 4.000000E-01 9.000000E-01
 1353009 5.000000E-01 9.700000E-01
 1353010 8.000000E-01 9.000000E-01
 1353011 9.000000E-01 8.000000E-01
 1353012 9.600000E-01 5.000000E-01
 1353013 1.000000E+00 0.000000E+00

 * TORQUE CURVE
 *

1353100 0 0
 1353101 0.000000E+00 0.000000E+00
 1353102 1.200000E-01 7.000000E-02
 1353103 1.650000E-01 1.250000E-01
 1353104 2.400000E-01 5.600000E-01
 1353105 8.000000E-01 5.800000E-01
 1353106 9.600000E-01 4.500000E-01
 1353107 1.000000E+00 0.000000E+00

 * PUMP 2-PHASE DIFFERENCE DATA
 *

 * HEAD CURVE NO. 1
 *

1354100 1 1
 1354101 0.000000E+00 0.000000E+00
 1354102 1.000000E-01 8.300000E-01
 1354103 2.000000E-01 1.090000E+00
 1354104 5.000000E-01 1.070000E+00
 1354105 7.000000E-01 1.010000E+00
 1354106 9.000000E-01 9.400000E-01
 1354107 1.000000E+00 1.000000E+00

 * HEAD CURVE NO. 2
 *

1354200 1 2
 1354201 0.000000E+00 0.000000E+00

1354300 1 3
 1354301 -1.000000E+00 -1.160000E+00
 1354302 -9.000000E-01 -1.740000E+00
 1354303 -8.000000E-01 -1.770000E+00
 1354304 -7.000000E-01 -2.360000E+00
 1354305 -6.000000E-01 -2.790000E+00
 1354306 -5.000000E-01 -2.910000E+00
 1354307 -4.000000E-01 -2.670000E+00
 1354308 -2.500000E-01 -1.590000E+00
 1354309 -1.000000E-01 -5.000000E-01
 1354310 0.000000E+00 0.000000E+00

 * HEAD CURVE NO. 3
 *

1354400 1 4
 1354401 -1.000000E+00 -1.160000E+00
 1354402 -9.000000E-01 -1.740000E+00
 1354403 -8.000000E-01 -1.770000E+00
 1354404 -7.000000E-01 -2.360000E+00
 1354405 -6.000000E-01 -2.790000E+00
 1354406 -5.000000E-01 -2.910000E+00
 1354407 -4.000000E-01 -2.670000E+00
 1354408 -2.500000E-01 -1.590000E+00
 1354409 -1.000000E-01 -5.000000E-01
 1354410 0.000000E+00 0.000000E+00

 * HEAD CURVE NO. 4
 *

1354500 1 5
 1354501 0.130000E+00 0.000000E+00
 1354502 2.000000E-01 -2.400000E-01
 1354503 4.000000E-01 -4.300000E-01
 1354504 6.000000E-01 -9.300000E-01
 1354505 8.000000E-01 -1.190000E+00
 1354506 1.000000E+00 -1.470000E+00

 * HEAD CURVE NO. 5
 *

1354600 1 6
 1354601 0.000000E+00 1.000000E-01
 1354602 1.000000E-01 1.300000E-01
 1354603 2.000000E-01 1.500000E-01
 1354604 4.000000E-01 1.300000E-01
 1354605 5.000000E-01 7.000000E-02
 1354606 6.000000E-01 -4.000000E-02
 1354607 7.000000E-01 -2.300000E-01
 1354608 8.000000E-01 -5.100000E-01
 1354609 9.000000E-01 -9.100000E-01
 1354610 1.000000E+00 -1.470000E+00

 * HEAD CURVE NO. 6
 *

1354700 1 7
 1354701 -1.000000E+00 0.000000E+00
 1354702 0.000000E+00 0.000000E+00

 * HEAD CURVE NO. 8
 *

1354801 1 8
 1354801 -1.000000E+00 0.000000E+00
 1354802 0.000000E+00 0.000000E+00

 * TORQUE CURVE NO. 1
 *

1354900 2 1
 1354901 0.000000E+00 6.732000E-01
 1354902 1.500000E-01 8.325000E-01
 1354903 3.000000E-01 7.369000E-01
 1354904 5.955200E-01 8.331000E-01
 1354905 7.978200E-01 9.279000E-01
 1354906 1.000000E+00 1.000000E+00

 * TORQUE CURVE NO. 2
 *

1355000 2 3
 1355001 0.000000E+00 -6.700000E-01
 1355002 4.000000E-01 -2.577000E-01
 1355003 5.000000E-01 1.507000E-01
 1355004 7.372500E-01 5.268600E-01
 1355005 7.680400E-01 6.065940E-01
 1355006 8.672300E-01 7.836600E-01
 1355007 1.000000E+00 1.000000E+00

 * TORQUE CURVE NO. 3
 *

1355100 2 3
 1355101 -1.000000E+00 1.984300E+00
 1355102 -8.009600E-01 1.384000E+00
 1355103 -5.063800E-01 1.091500E+00
 1355104 -4.068000E-01 8.220000E-01
 1355105 -1.992800E-01 6.848000E-01
 1355106 0.000000E+00 6.020000E-01

 * TORQUE CURVE NO. 4
 *

1355200 2 4
 1355201 -1.000000E+00 1.584300E+00
 1355202 -8.773400E-01 1.030800E+00
 1355203 -6.337100E-01 1.682400E+00
 1355204 -4.585300E-01 1.557000E+00
 1355205 -2.870230E-01 1.435200E+00
 1355206 -1.761070E-01 1.387900E+00
 1355207 -8.931000E-02 1.348100E+00
 1355208 0.000000E+00 1.233610E+00

 * TORQUE CURVE NO. 5
 *

1355300 2 5
 1355301 0.000000E+00 -4.500000E-01
 1355302 4.000000E-01 -2.500000E-01
 1355303 5.000000E-01 0.000000E+00
 1355304 1.000000E+00 2.500000E-01

 * TORQUE CURVE NO. 6
 *

1355400 2 6
 1355401 0.000000E+00 1.233610E+00
 1355402 9.064300E-02 1.196400E+00
 1355403 1.885600E-01 1.109800E+00
 1355404 2.734700E-01 1.041600E+00

1987-06-03

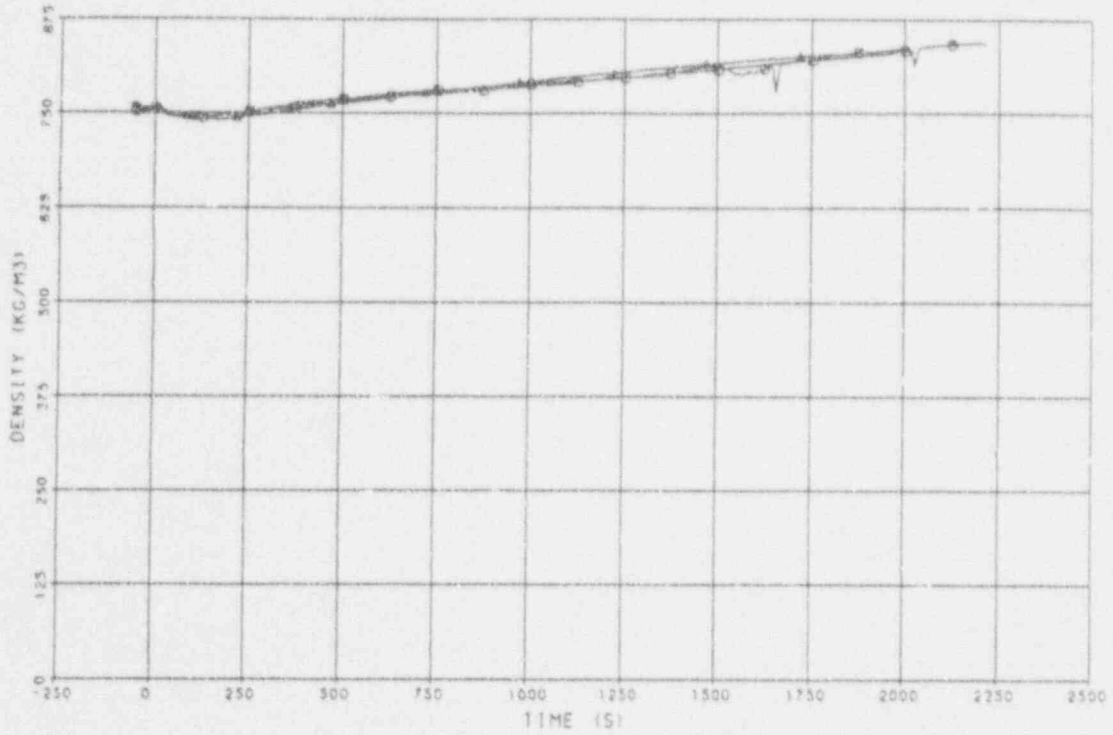
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5100103	90.0			1				
5100104	0.0			2				
5100105	4.E-5			0.4				
5100106	0.4			0.4				
5100107	0.000			1				
5100108	0.0			1				
5100109	0.0			1				
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510028								

Data Comparison Plots

1987-06-09

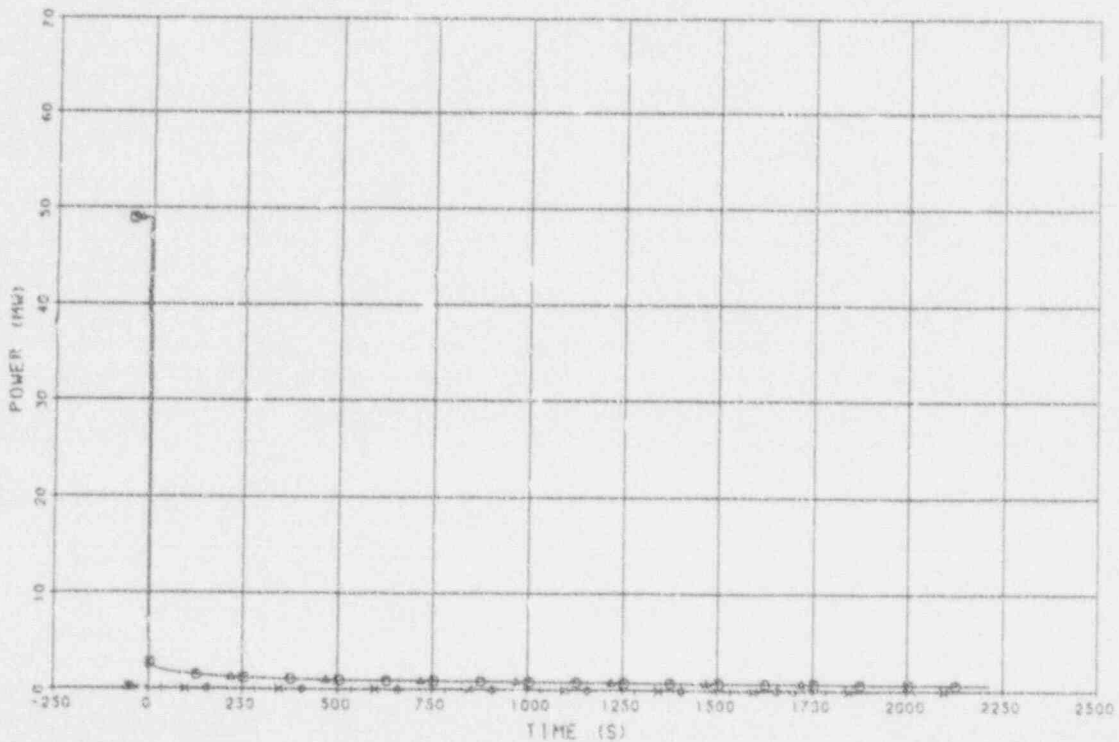
* CORE INLET FLUID DENSITY (CNTRLVAR 901) CASE A
 * CORE INLET FLUID DENSITY (CNTRLVAR 901) CASE B
 * CORE INLET FLUID DENSITY (CNTRLVAR 901) CASE C

Plot B. 1



* REACTOR POWER (RNTPWR D) CASE A
 * REACTOR POWER (RNTPWR D) CASE B
 * REACTOR POWER (RNTPWR D) CASE C
 * PRIM EXTERNALS HEAT FLOW (CNTRLVAR 992) CASE A
 * PRIM EXTERNALS HEAT FLOW (CNTRLVAR 992) CASE B
 * PRIM EXTERNALS HEAT FLOW (CNTRLVAR 992) CASE C

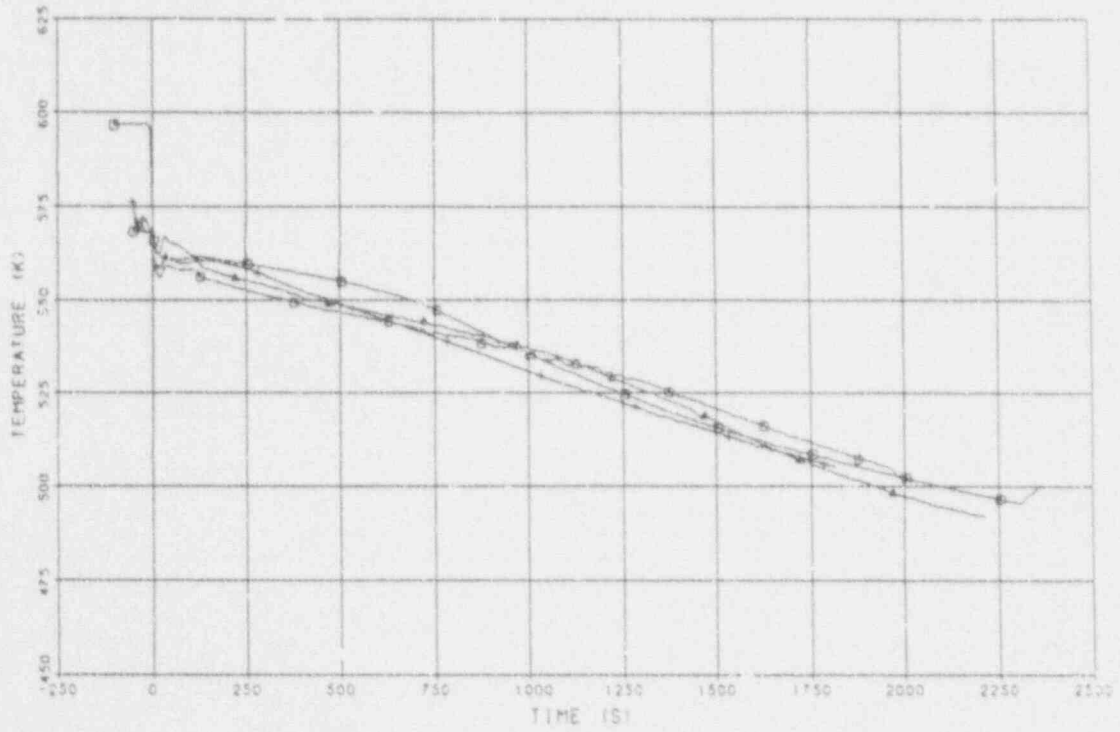
Plot B. 2



1987-06-09

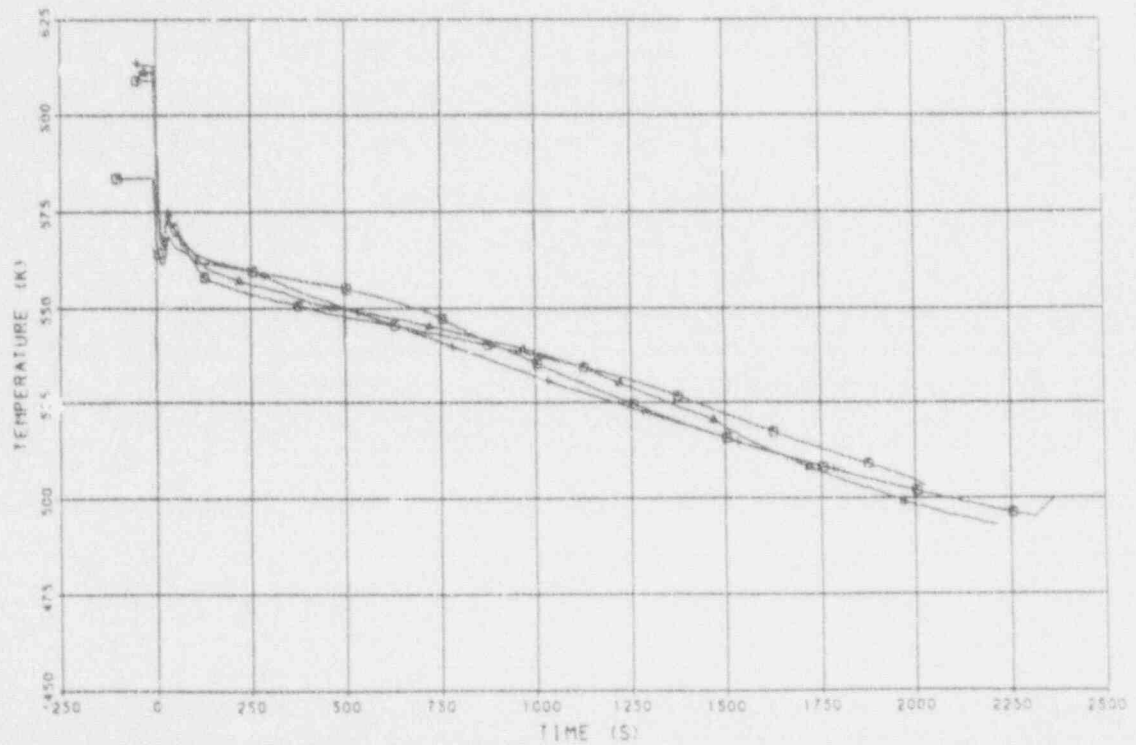
4 8 0 0 3 CORE CLAD TEMPERATURE VOL 1 (TE-26-4-011) EXP
 4 8 0 0 3 CORE CLAD TEMPERATURE VOL 1 (CNTRLVAR 903) CASE A
 4 8 0 0 3 CORE CLAD TEMPERATURE VOL 1 (CNTRLVAR 903) CASE B
 4 8 0 0 3 CORE CLAD TEMPERATURE VOL 1 (CNTRLVAR 903) CASE C

Plot B. 3



4 8 0 0 3 CORE CLAD TEMPERATURE VOL 1 (TE-177-015) EXP
 4 8 0 0 3 CORE CLAD TEMPERATURE VOL 1 (CNTRLVAR 904) CASE A
 4 8 0 0 3 CORE CLAD TEMPERATURE VOL 1 (CNTRLVAR 904) CASE B
 4 8 0 0 3 CORE CLAD TEMPERATURE VOL 1 (CNTRLVAR 904) CASE C

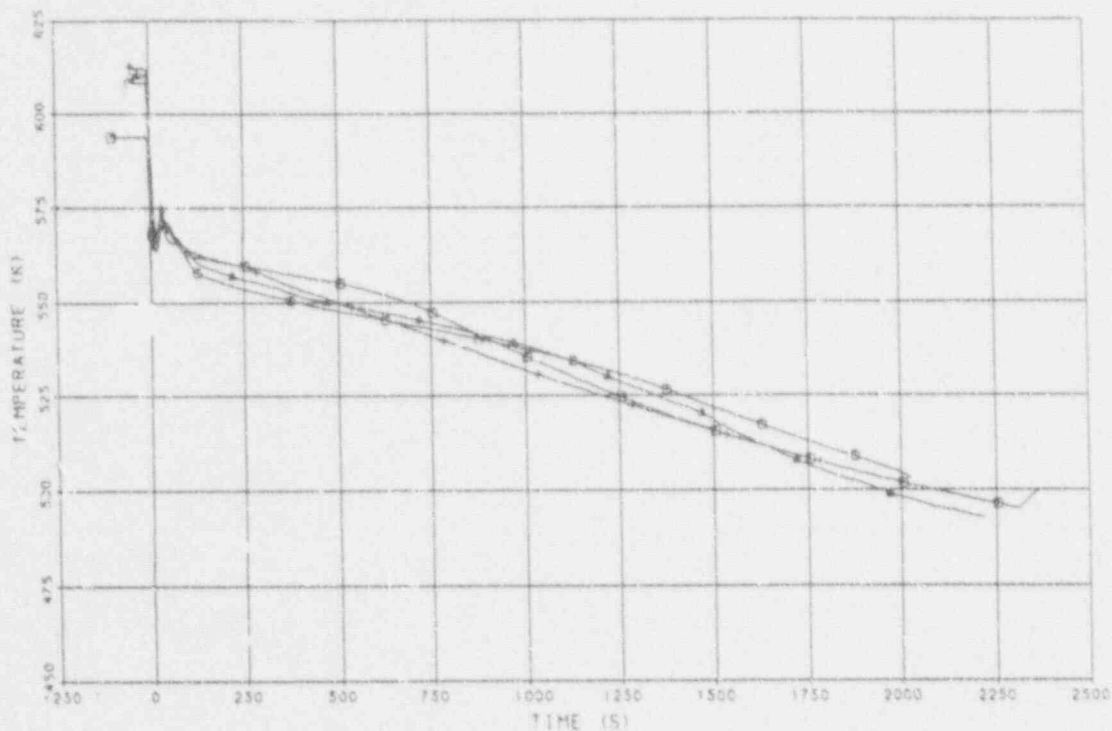
Plot B. 4



1987-06-09

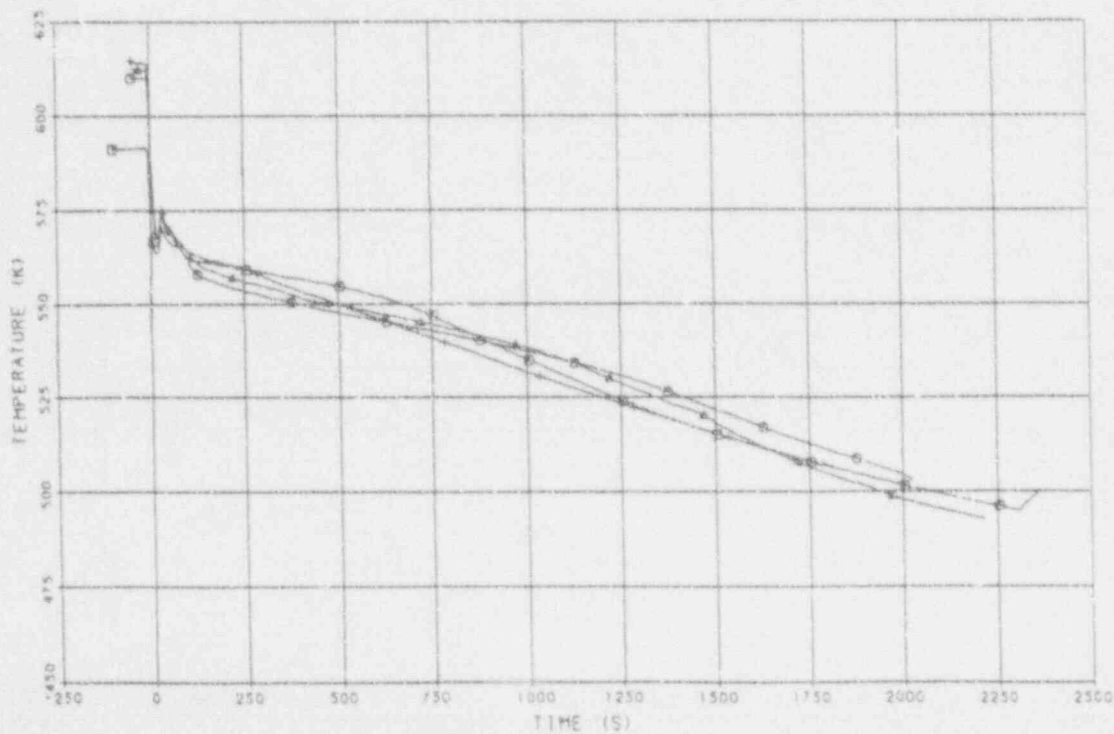
+ 800 CORE CLAD TEMPERATURE YOL 3 (TE-1F7-026) 1 EXP
 CORE CLAD TEMPERATURE YOL 3 (CNTRLVAR 905) CASE A
 CORE CLAD TEMPERATURE YOL 3 (CNTRLVAR 905) CASE B
 CORE CLAD TEMPERATURE YOL 3 (CNTRLVAR 905) CASE C

Plot B. 5



+ 810 CORE CLAD TEMPERATURE YOL 4 (TE-2008-039) EXP
 CORE CLAD TEMPERATURE YOL 4 (CNTRLVAR 906) CASE A
 CORE CLAD TEMPERATURE YOL 4 (CNTRLVAR 906) CASE B
 CORE CLAD TEMPERATURE YOL 4 (CNTRLVAR 906) CASE C

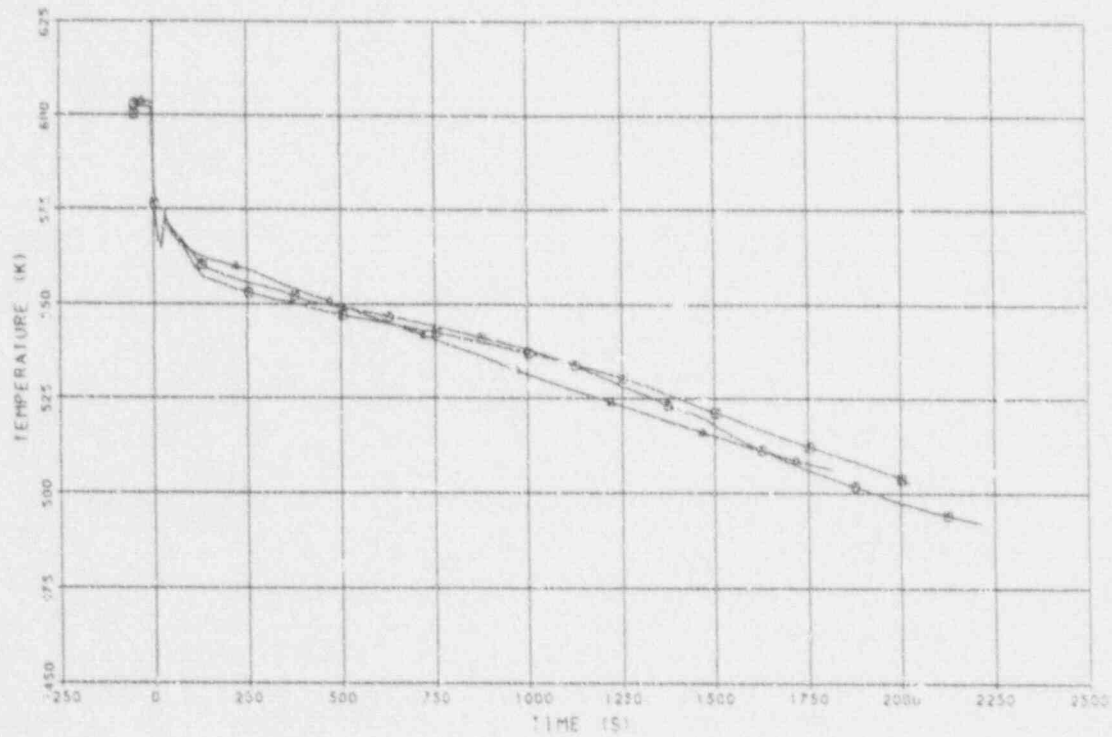
Plot B. 6



1987-06-09

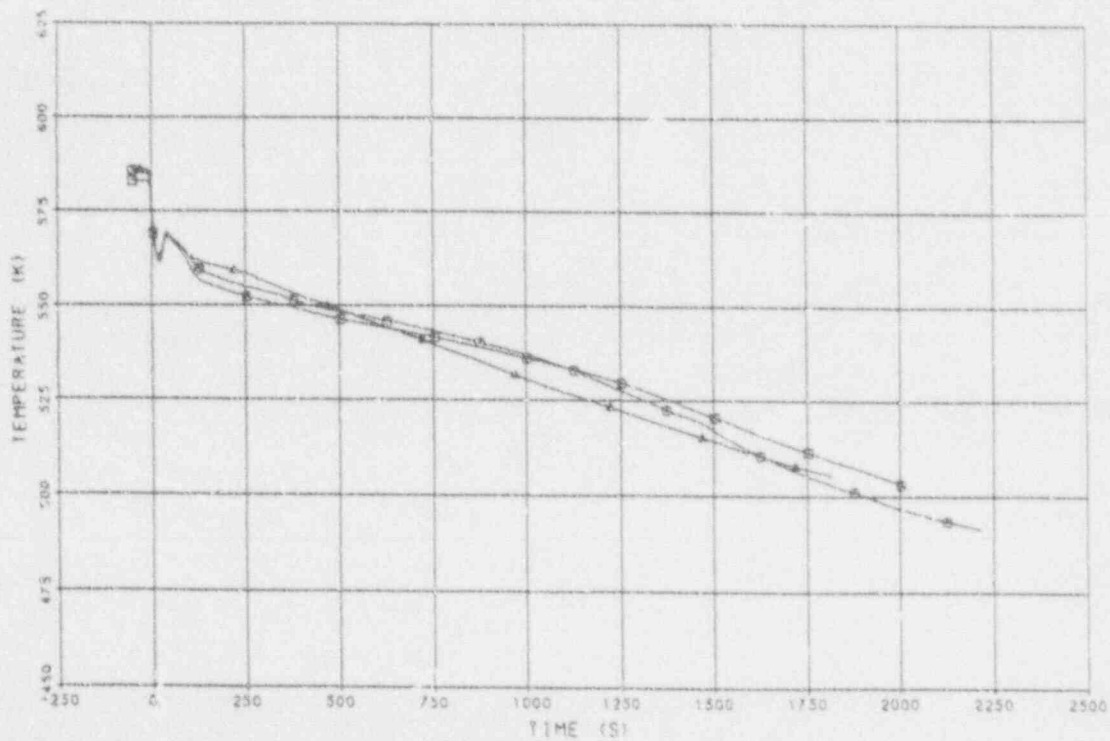
* 00 CORE CLAD TEMPERATURE VOL 5 ICNTRLYAR 9071 CASE A
 * 00 CORE CLAD TEMPERATURE VOL 5 ICNTRLYAR 9071 CASE B
 * 00 CORE CLAD TEMPERATURE VOL 5 ICNTRLYAR 9071 CASE C

Plot B. 7



* 00 CORE CLAD TEMPERATURE VOL 6 ICNTRLYAR 9081 CASE A
 * 00 CORE CLAD TEMPERATURE VOL 6 ICNTRLYAR 9081 CASE B
 * 00 CORE CLAD TEMPERATURE VOL 6 ICNTRLYAR 9081 CASE C

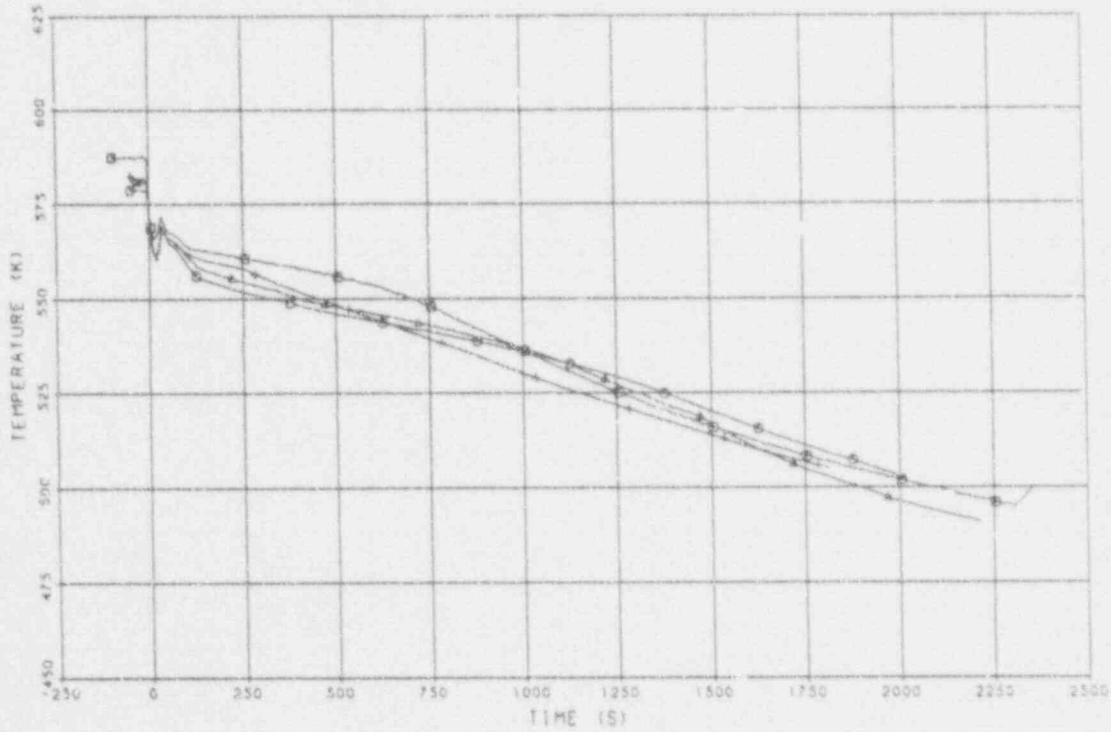
Plot B. 8



1987-06-09

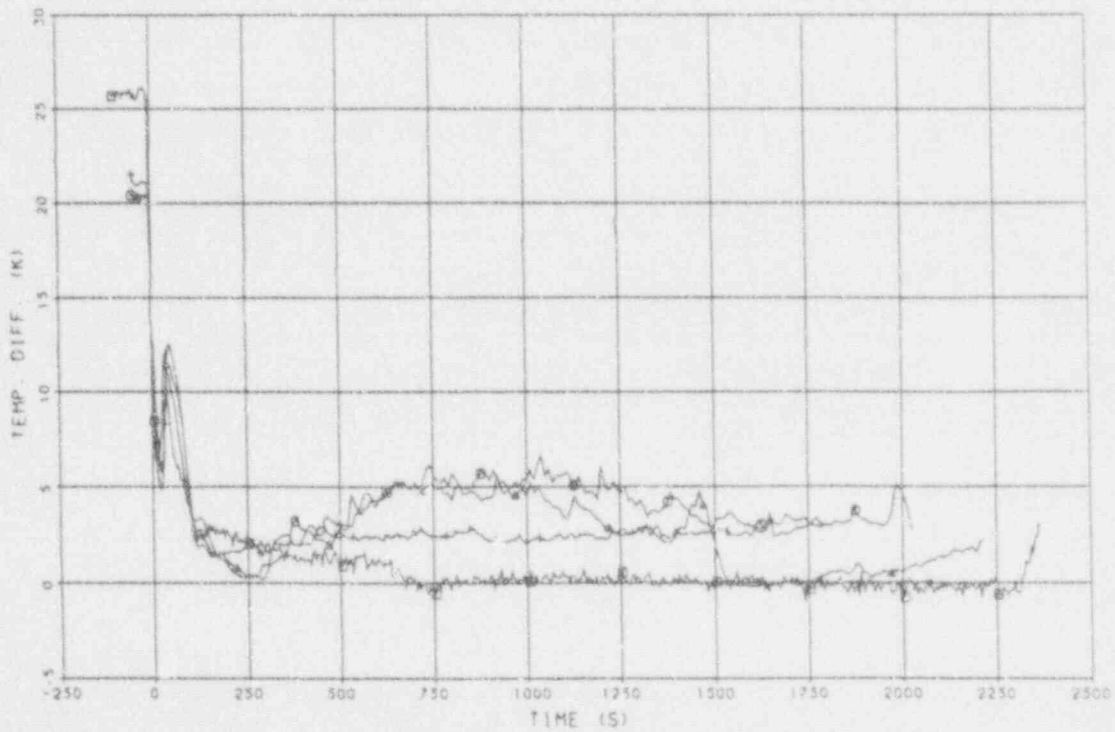
* 400 CORE OUTLET TEMPERATURE (TE-1UP-001) EXP
 * 400 CORE OUTLET TEMPERATURE (CNTRLVAR 900) CASE A
 * 400 CORE OUTLET TEMPERATURE (CNTRLVAR 900) CASE B
 * 400 CORE OUTLET TEMPERATURE (CNTRLVAR 900) CASE C

Plot B.9



* 400 CORE FLUID TEMPERATURE DIFF (TE-1UP-001 - TE-1LW-001) EXP
 * 400 CORE FLUID TEMPERATURE DIFF (CNTRLVAR 910) CASE A
 * 400 CORE FLUID TEMPERATURE DIFF (CNTRLVAR 910) CASE B
 * 400 CORE FLUID TEMPERATURE DIFF (CNTRLVAR 910) CASE C

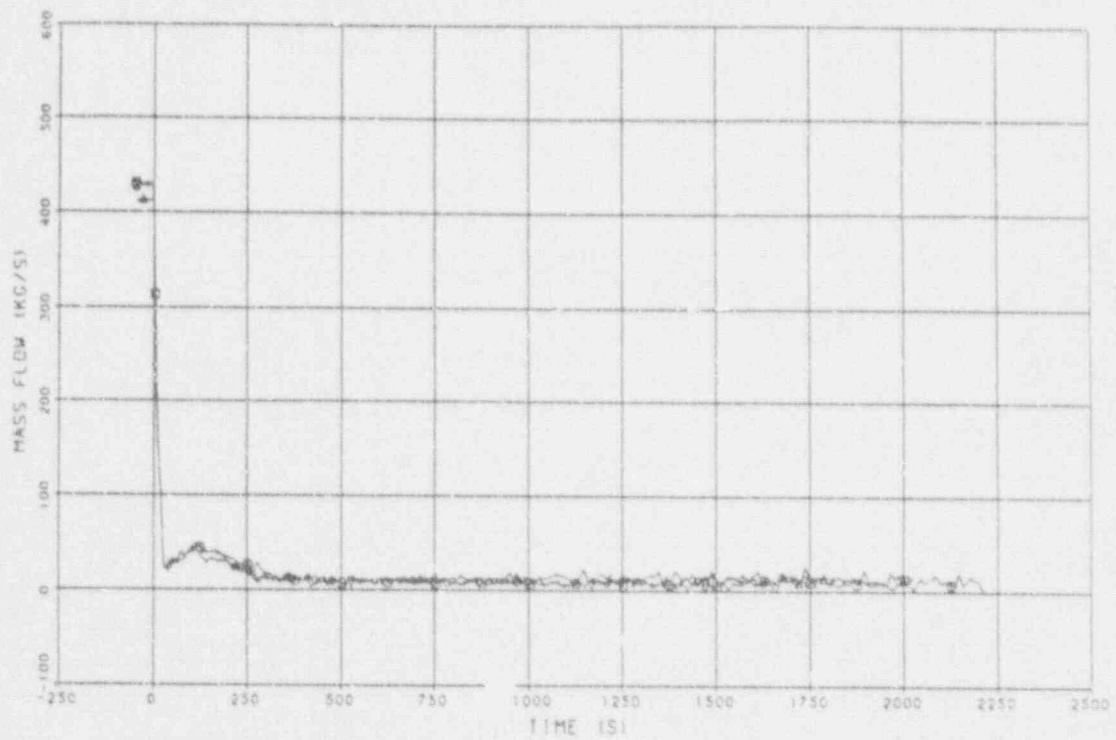
Plot B.10



1987-06-09

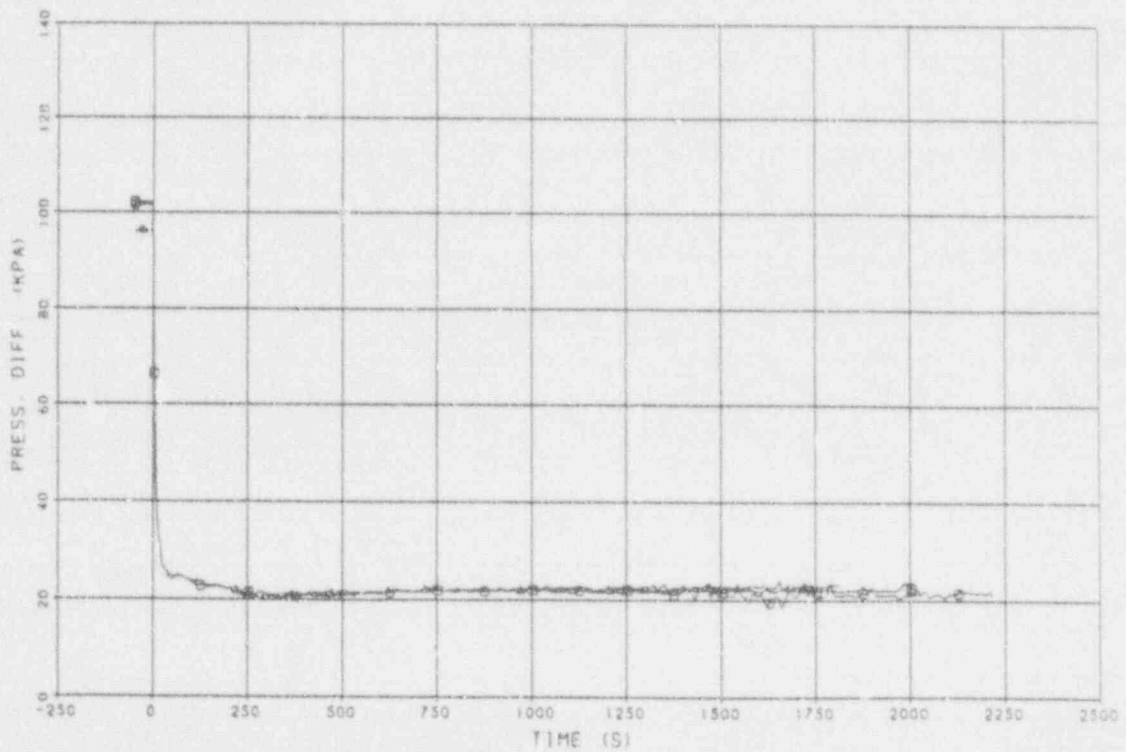
*00 CORE INLET MASS FLOW (MFLWJ 225) CASE A
*00 CORE INLET MASS FLOW (MFLWJ 225) CASE B
*00 CORE INLET MASS FLOW (MFLWJ 225) CASE C

Plot B.11



*00 CORE MASS INVENTORY (CNTRLVAR 912) CASE A
*00 CORE MASS INVENTORY (CNTRLVAR 912) CASE B
*00 CORE MASS INVENTORY (CNTRLVAR 912) CASE C

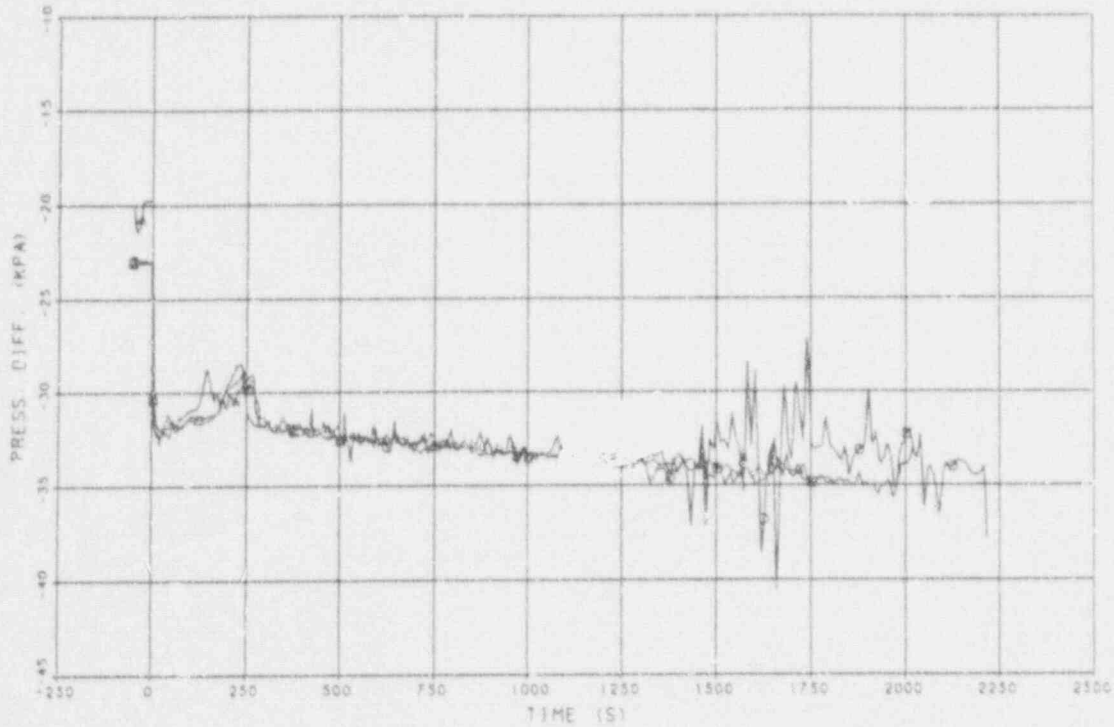
Plot B.12



1987-06-09

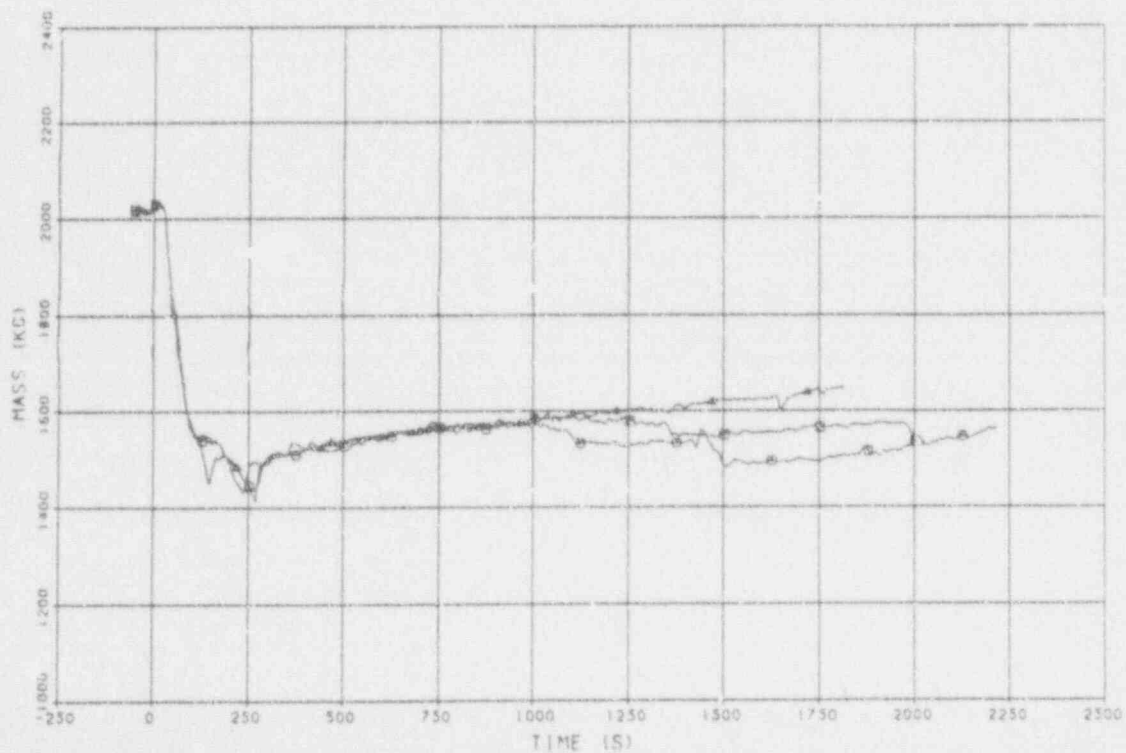
B0 DOWNCOMER MASS INVENTORY (CTRLVAR 9:3) CASE A
DOWNCOMER MASS INVENTORY (CTRLVAR 9:3) CASE B
A DOWNCOMER MASS INVENTORY (CTRLVAR 9:3) CASE C

Plot B.13



B0 VESSEL TOTAL MASS INVENTORY (CTRLVAR 9:4) CASE A
VESSEL TOTAL MASS INVENTORY (CTRLVAR 9:4) CASE B
A VESSEL TOTAL MASS INVENTORY (CTRLVAR 9:4) CASE C

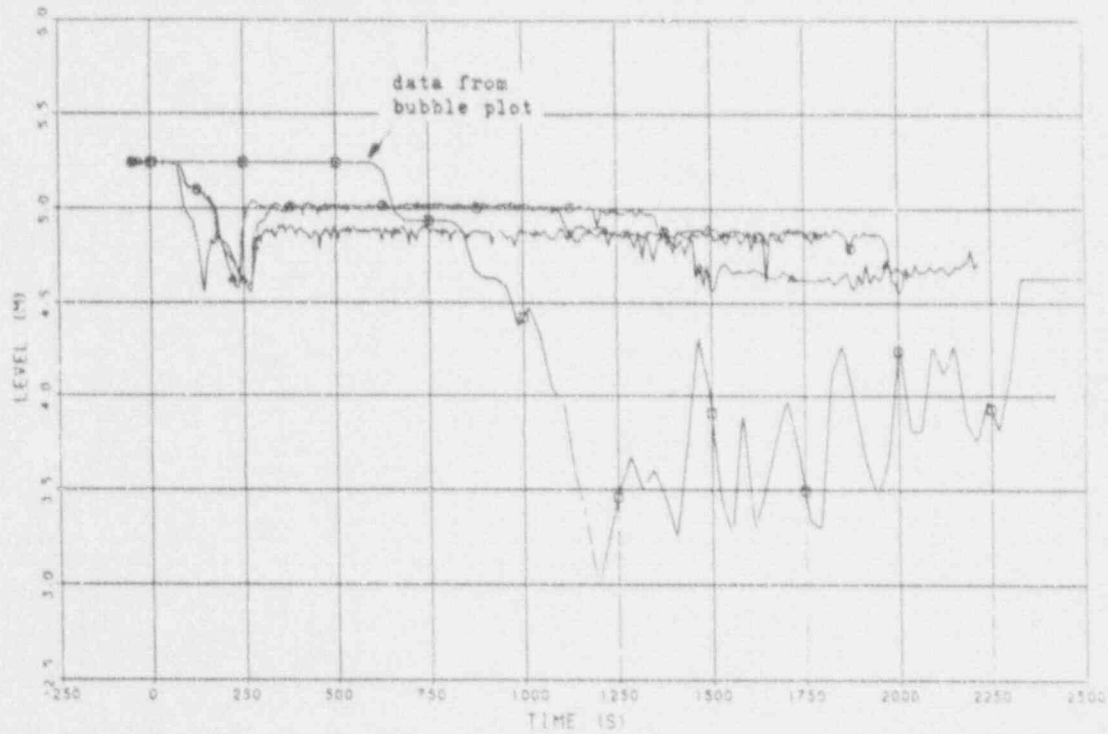
Plot B.14



1987-06-09

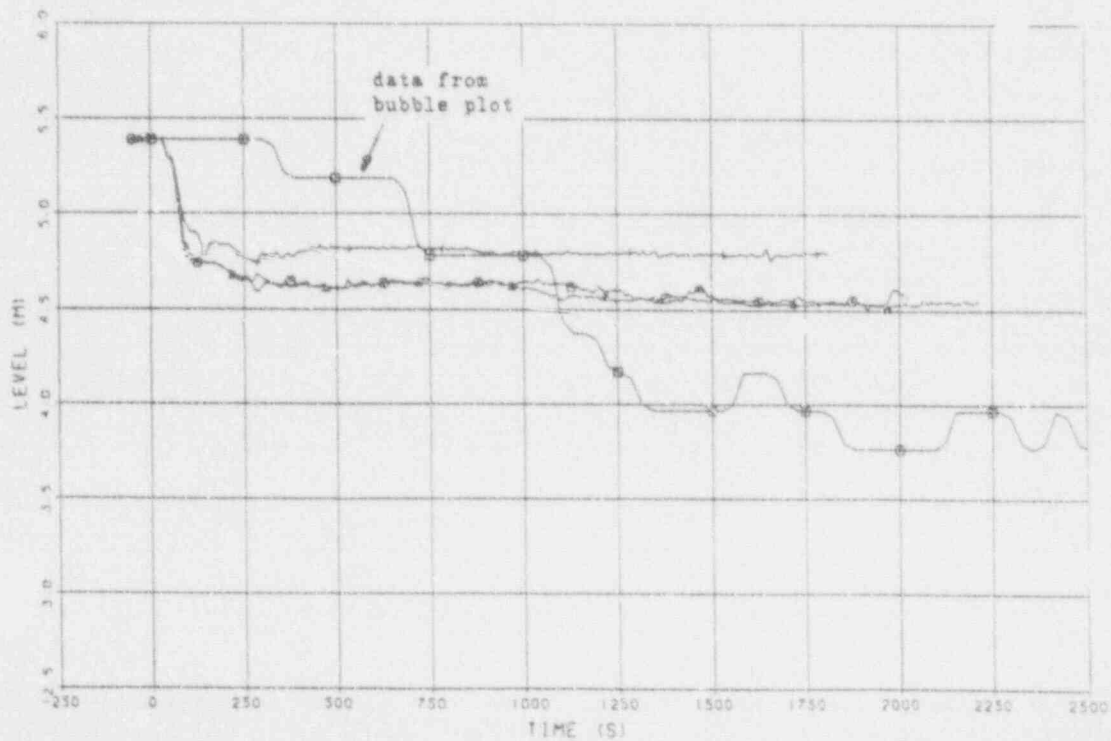
+ 400 DOWNCOMER LIQUID LEVEL (LE-ST-001) EXP
 + 400 DOWNCOMER LIQUID LEVEL (CNTRLVAR 915) CASE A
 + 400 DOWNCOMER LIQUID LEVEL (CNTRLVAR 915) CASE B
 + 400 DOWNCOMER LIQUID LEVEL (CNTRLVAR 915) CASE C

Plot B.15



+ 400 UPPER PLENUM LIQUID LEVEL (LE-SUP-001) EXP
 + 400 UPPER PLENUM LIQUID LEVEL (CNTRLVAR 916) CASE A
 + 400 UPPER PLENUM LIQUID LEVEL (CNTRLVAR 916) CASE B
 + 400 UPPER PLENUM LIQUID LEVEL (CNTRLVAR 916) CASE C

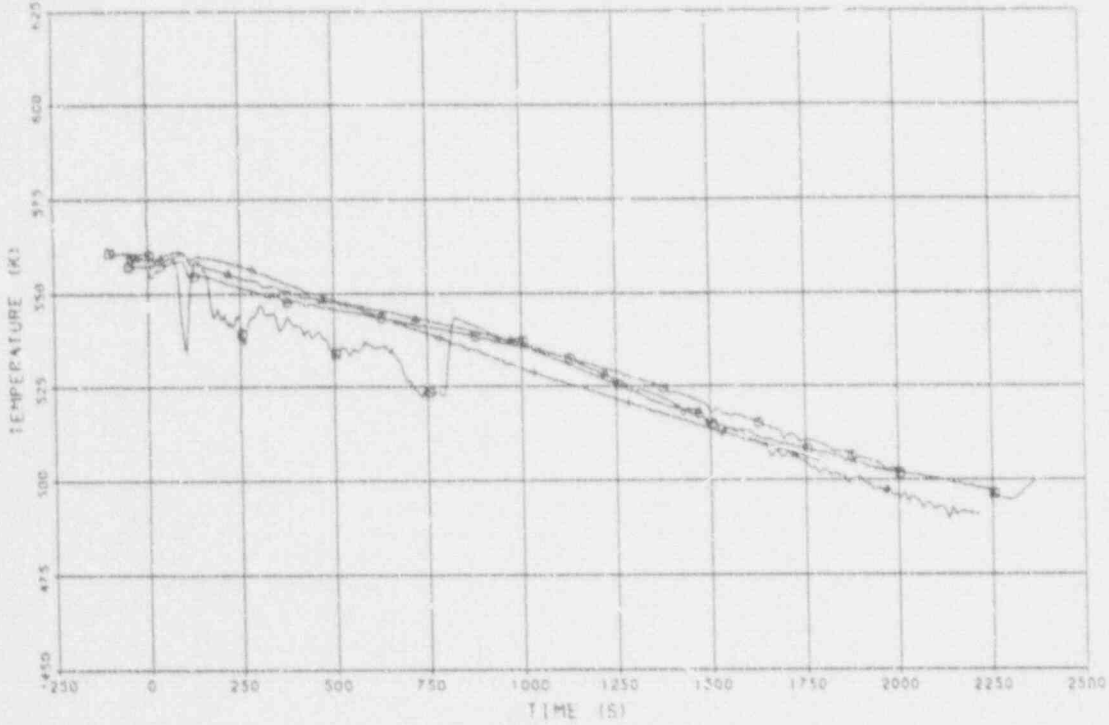
Plot B.16



1987-06-09

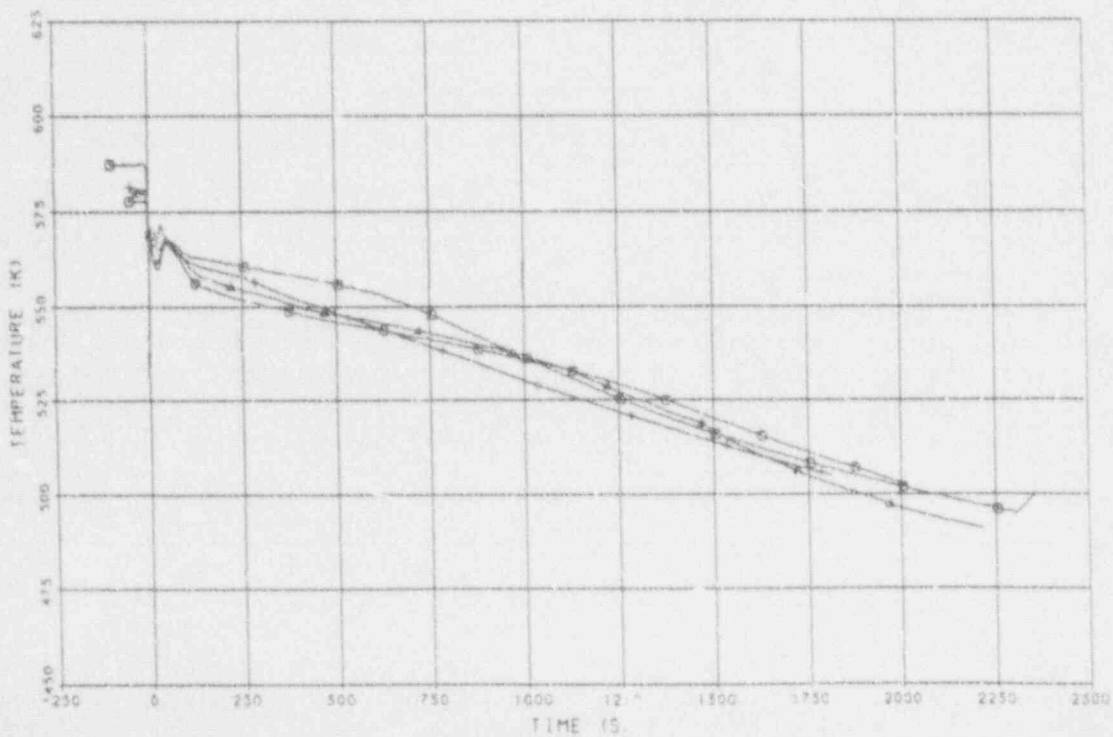
* DOWNCOMER INLET TEMPERATURE (ITE-101-001) EXP
 * DOWNCOMER INLET TEMPERATURE (TEMPF 205) CASE A
 * DOWNCOMER INLET TEMPERATURE (TEMPF 205) CASE B
 * DOWNCOMER INLET TEMPERATURE (TEMPF 205) CASE C

Plot B.17



* UPPER PLENUM TEMPERATURE (ITE-101-001) EXP
 * UPPER PLENUM TEMPERATURE (TEMPF 240) CASE A
 * UPPER PLENUM TEMPERATURE (TEMPF 240) CASE B
 * UPPER PLENUM TEMPERATURE (TEMPF 240) CASE C

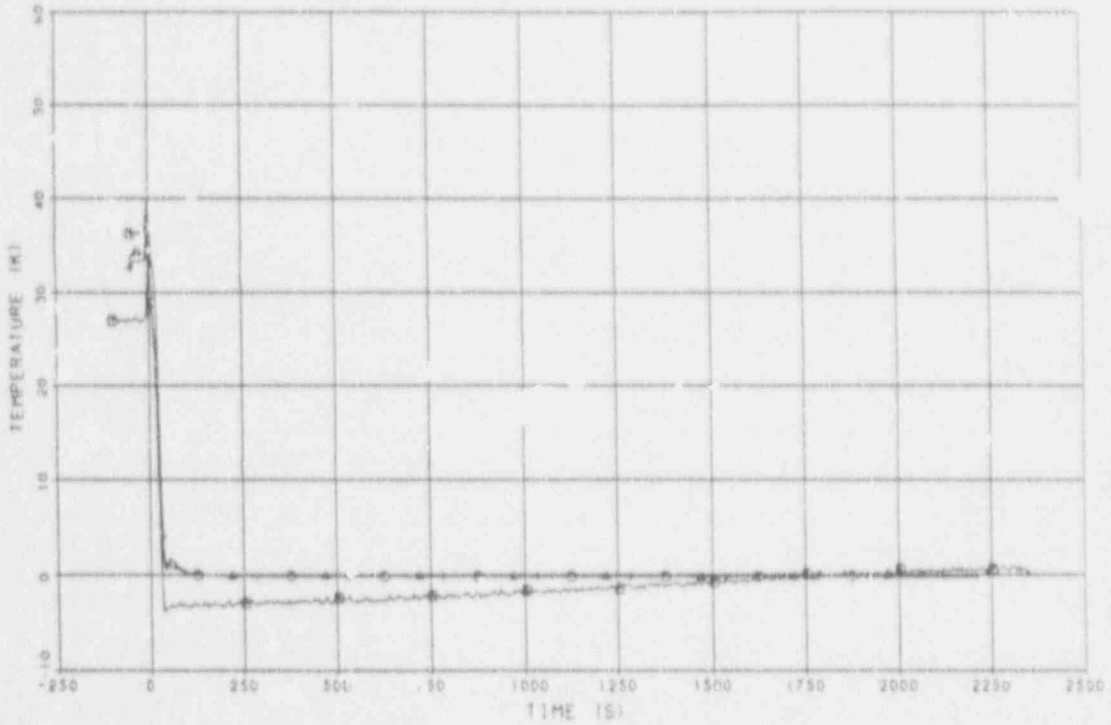
Plot B.18



1987-06-09

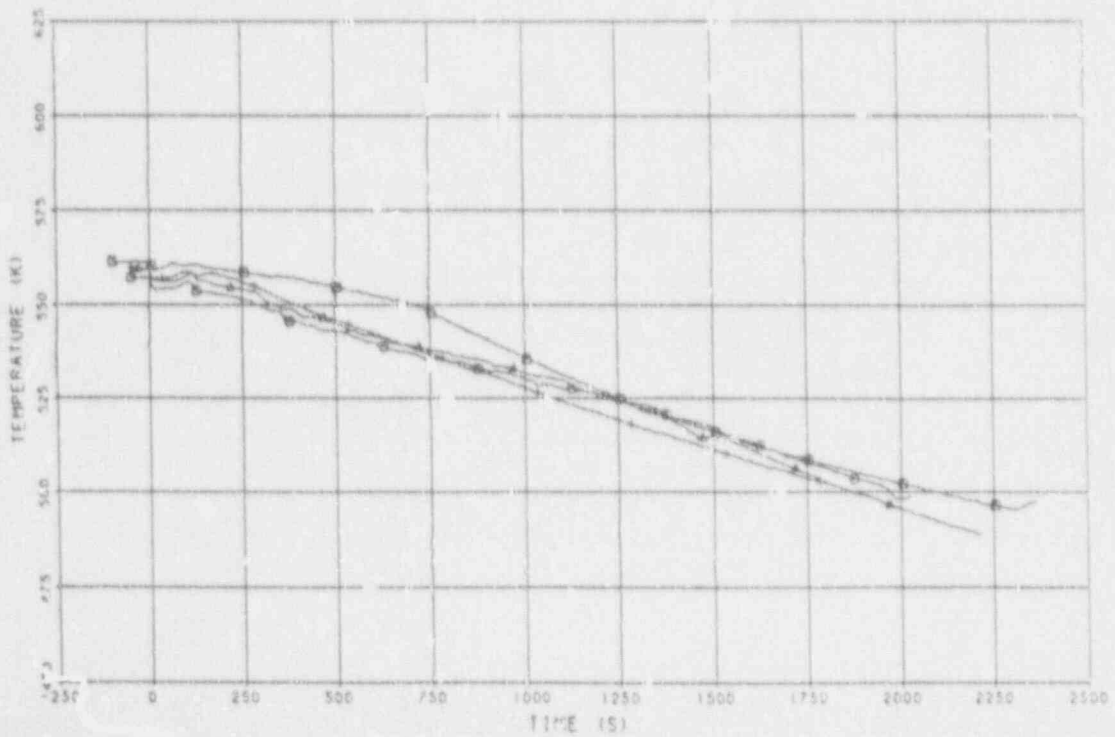
* 4 0 0 UPPER PLENUM SUBCOOLING (ST-UP-11) - (TE-UP-001) EXP.
 UPPER PLENUM SUBCOOLING (CTRLVAR 918) CASE A
 UPPER PLENUM SUBCOOLING (CTRLVAR 919) CASE B
 UPPER PLENUM SUBCOOLING (CTRLVAR 910) CASE C

Plot B.19



* 4 0 0 LOWER PLENUM TEMPERATURE (TE-LLP-001) EXP.
 LOWER PLENUM TEMPERATURE (TEMP 225) CASE A
 LOWER PLENUM TEMPERATURE (TEMP 225) CASE B
 LOWER PLENUM TEMPERATURE (TEMP 225) CASE C

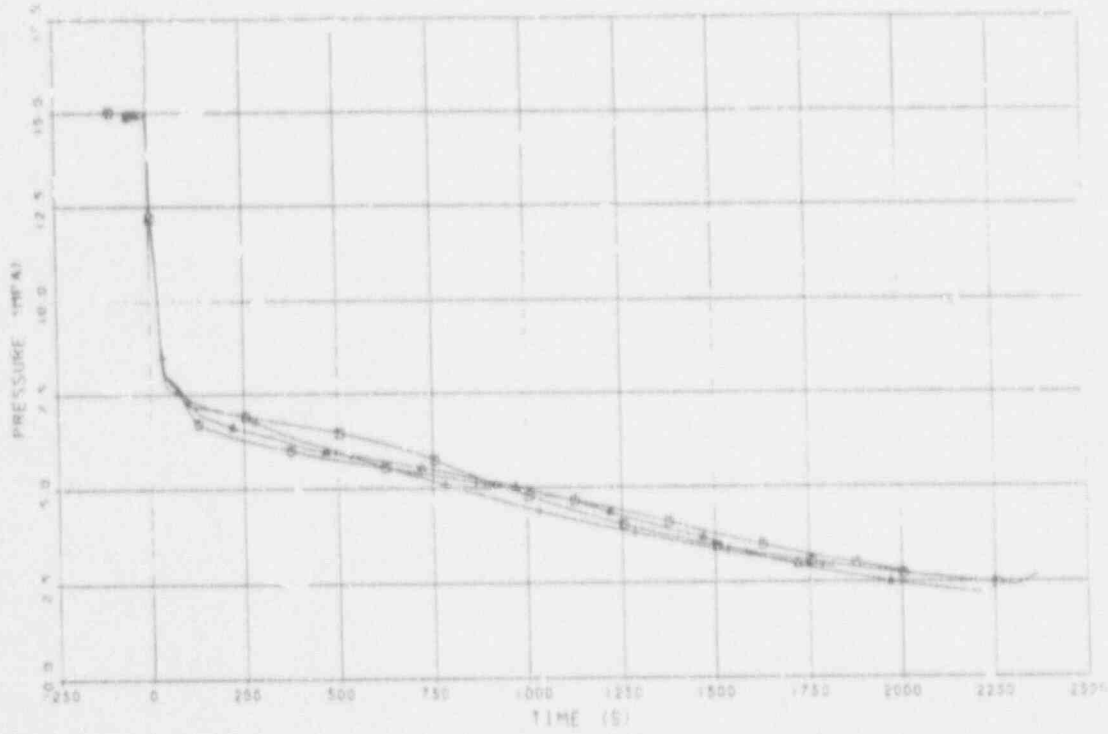
Plot B.20



1987-06-09

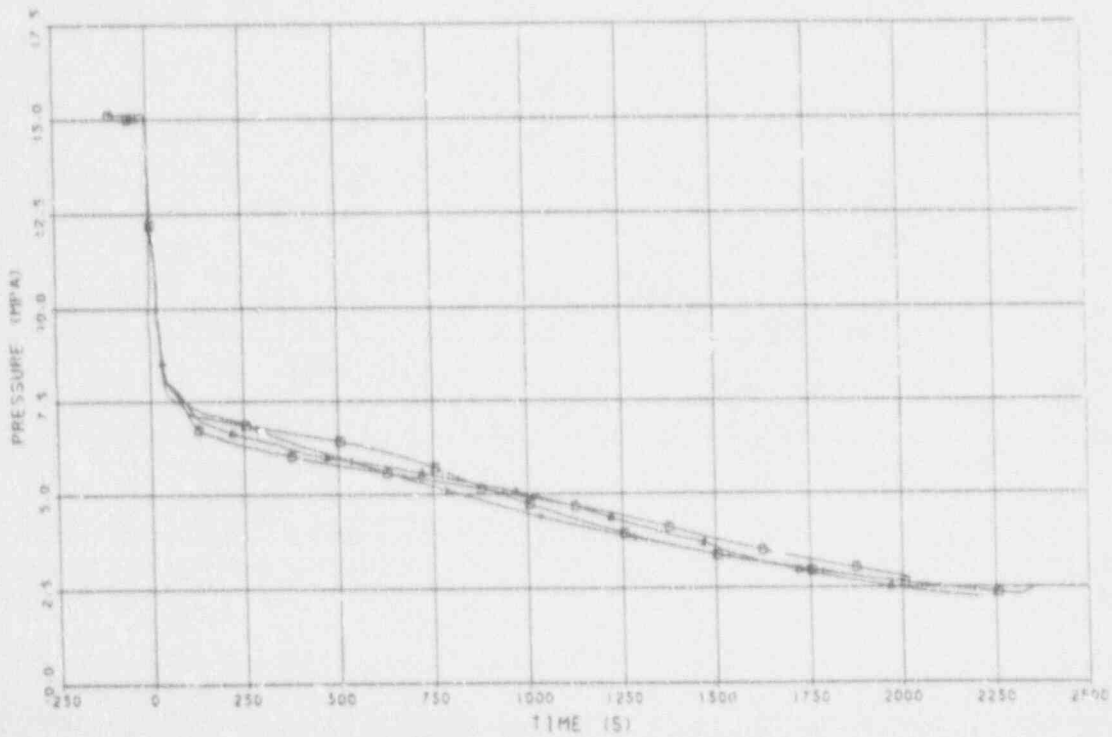
4800 UPPER PLENUM PRESSURE (PE-1UP-001A) EXP.
 4800 UPPER PLENUM PRESSURE (P 245) CASE A
 4800 UPPER PLENUM PRESSURE (P 245) CASE B
 4800 UPPER PLENUM PRESSURE (P 245) CASE C

Plot B.21



4800 LOWER PLENUM PRESSURE (PE-1LT-001A) EXP.
 4800 LOWER PLENUM PRESSURE (P 225) CASE A
 4800 LOWER PLENUM PRESSURE (P 225) CASE B
 4800 LOWER PLENUM PRESSURE (P 225) CASE C

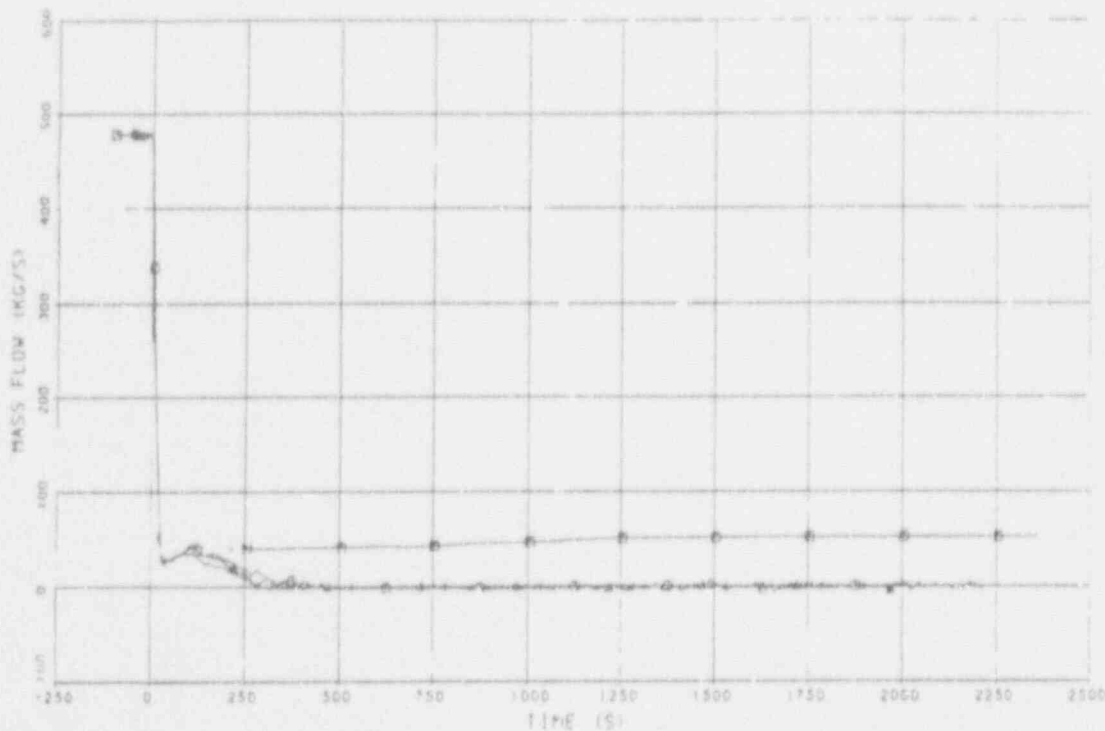
Plot B.22



1987-06-09

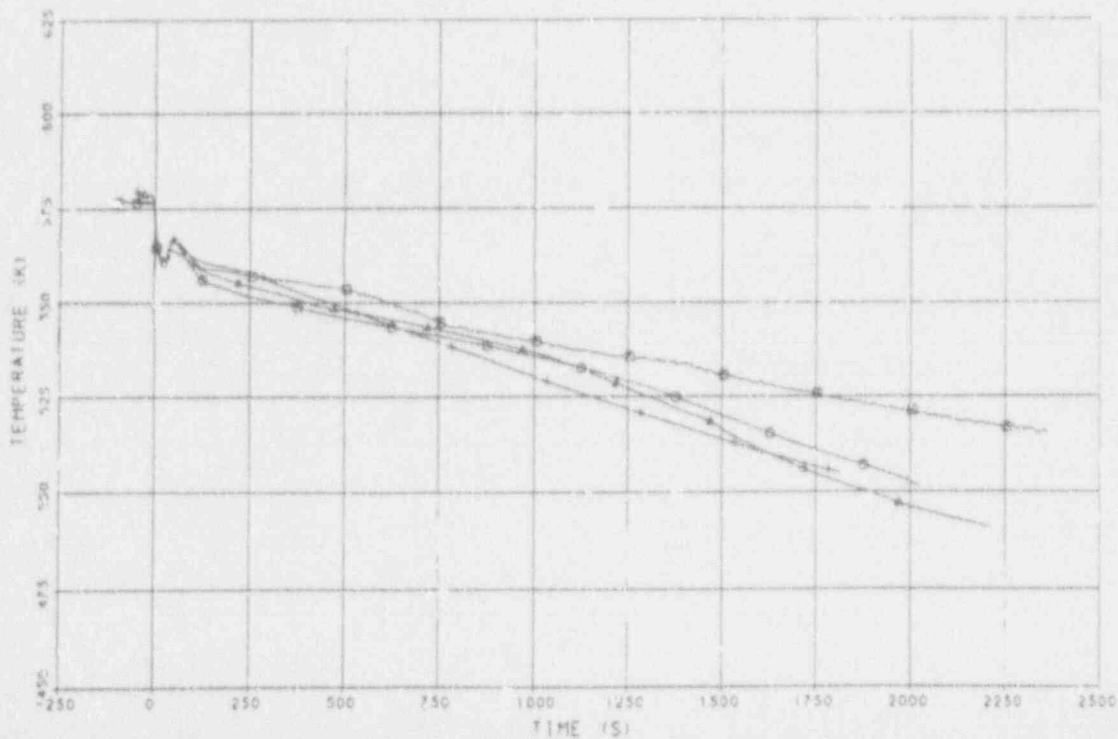
* * * * *
1.101 L-101 MASS FLOW RATE 101 101 101 101 EXP
1.102 L-102 MASS FLOW RATE 102 102 102 102 CASE A
1.103 L-103 MASS FLOW RATE 103 103 103 103 CASE B
1.104 L-104 MASS FLOW RATE 104 104 104 104 CASE C

Plot B.25



* * * * *
1.101 L-101 TEMPERATURE 101 101 101 101 EXP
1.102 L-102 TEMPERATURE 102 102 102 102 CASE A
1.103 L-103 TEMPERATURE 103 103 103 103 CASE B
1.104 L-104 TEMPERATURE 104 104 104 104 CASE C

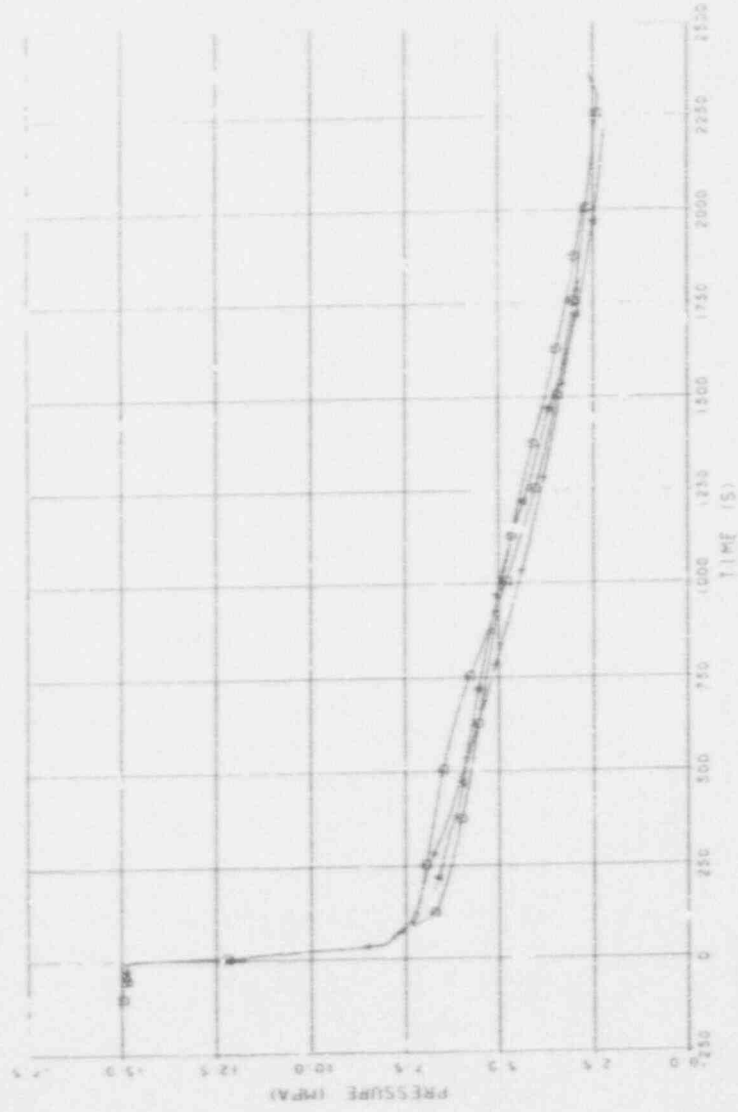
Plot B.26



1987-06-09

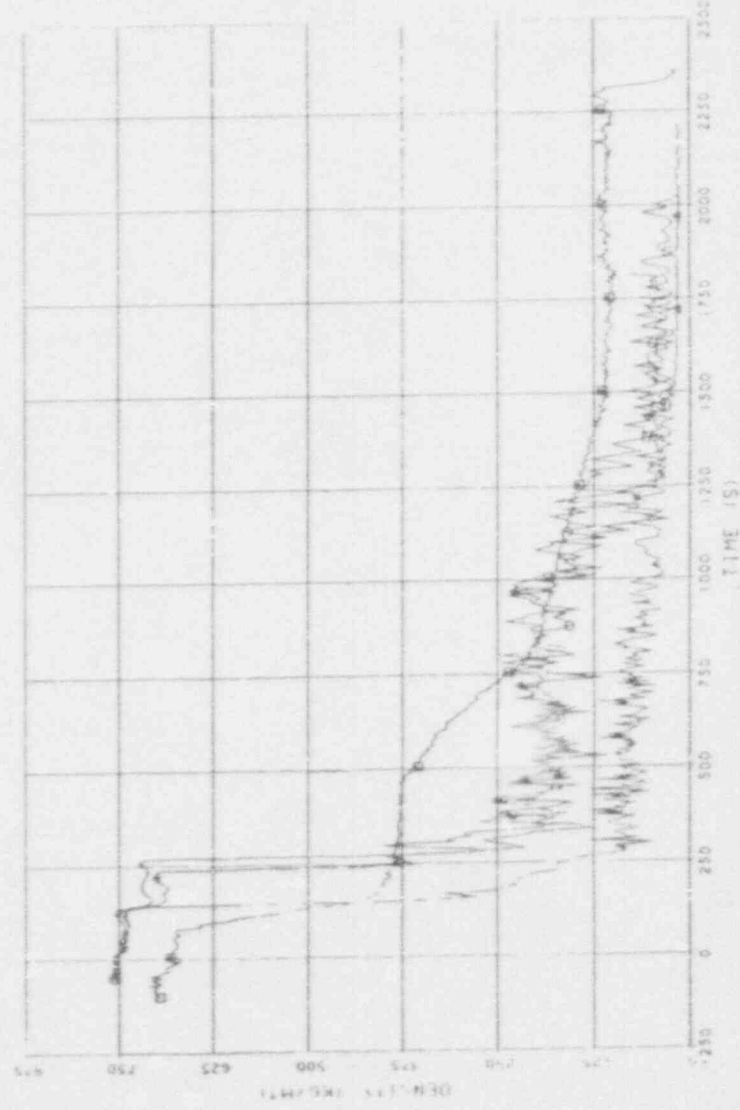
--- H01 LEG PRESSURE (PE-PC-002) - MPa
 --- H02 LEG PRESSURE (P-103) - CASE A
 --- H03 LEG PRESSURE (P-103) - CASE B
 --- H04 LEG PRESSURE (P-103) - CASE C

Plot B.27



--- C01 LEG FLUID DENSITY (DE-75-113) - G/KG
 --- C02 LEG FLUID DENSITY (RHO-183) - CASE A
 --- C03 LEG FLUID DENSITY (RHO-183) - CASE B
 --- C04 LEG FLUID DENSITY (RHO-183) - CASE C

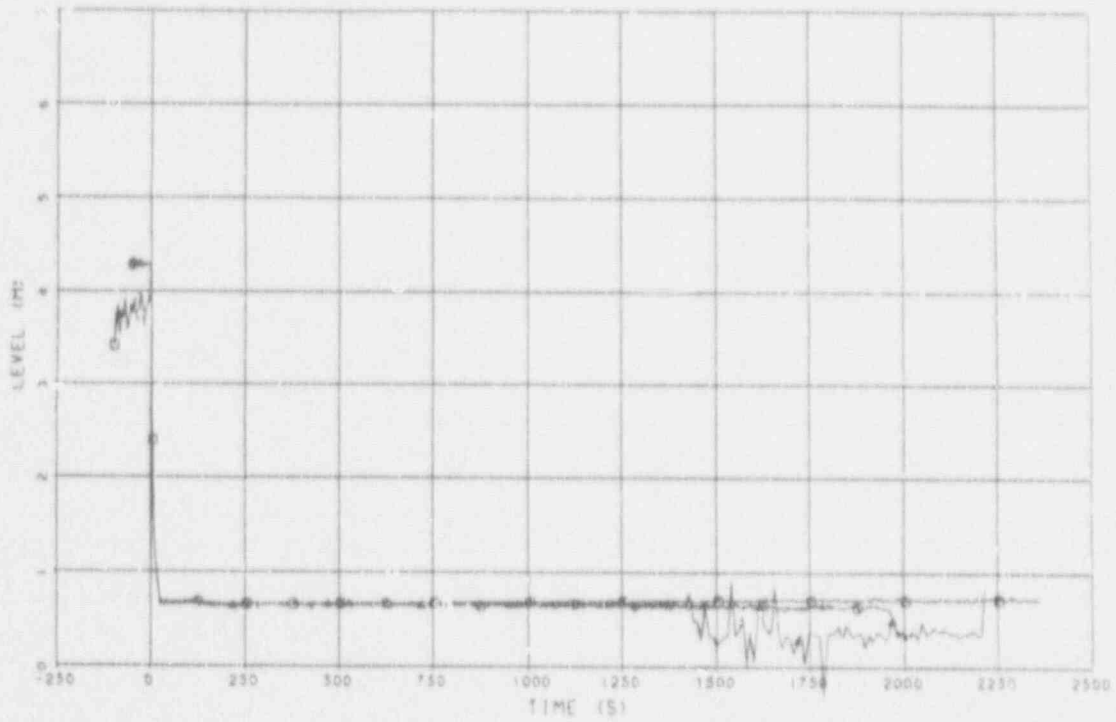
Plot B.28



1987-06-09

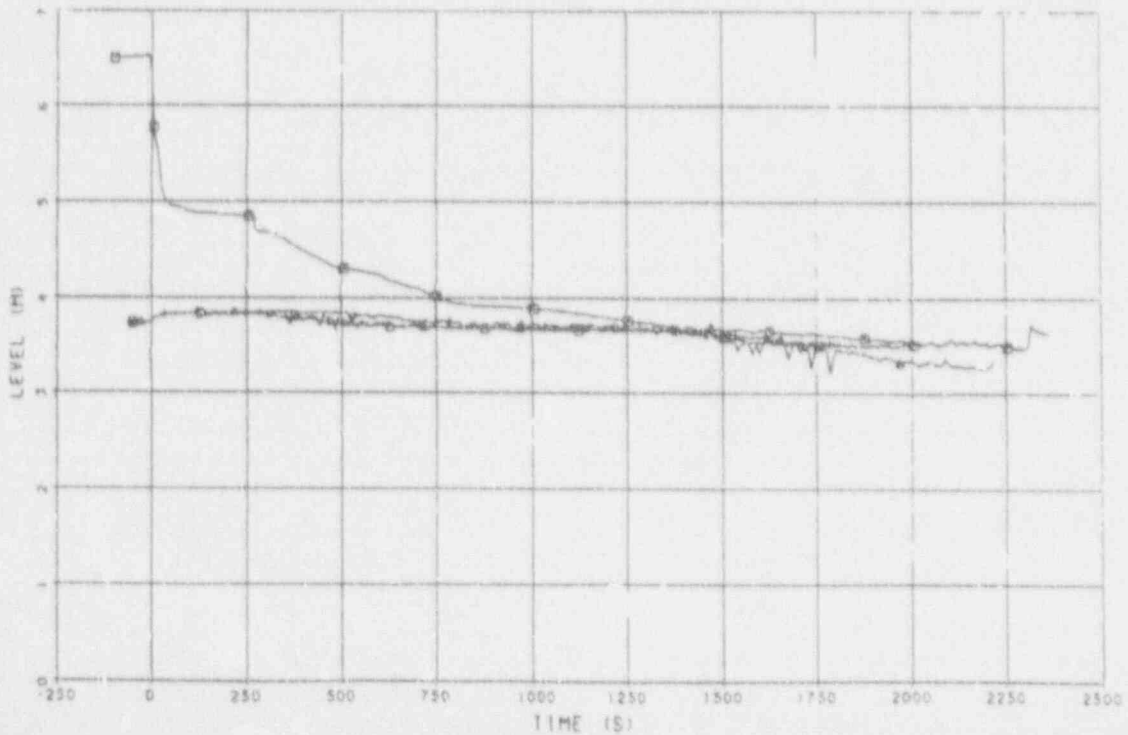
#00 1 L LOOP SEAL LIQUID LEVEL SLEPDE-PC-0281 EXP
 1 L LOOP SEAL LIQUID LEVEL (CENTR.VAR 931) CASE A
 1 L LOOP SEAL LIQUID LEVEL (CENTR.VAR 931) CASE B
 1 L LOOP SEAL LIQUID LEVEL (CENTR.VAR 931) CASE C

Plot B.31



#00 2 L LOOP SEAL LIQUID LEVEL SLEPDE-BL-0141 EXP
 2 L LOOP SEAL LIQUID LEVEL (CENTR.VAR 932) CASE A
 2 L LOOP SEAL LIQUID LEVEL (CENTR.VAR 932) CASE B
 2 L LOOP SEAL LIQUID LEVEL (CENTR.VAR 932) CASE C

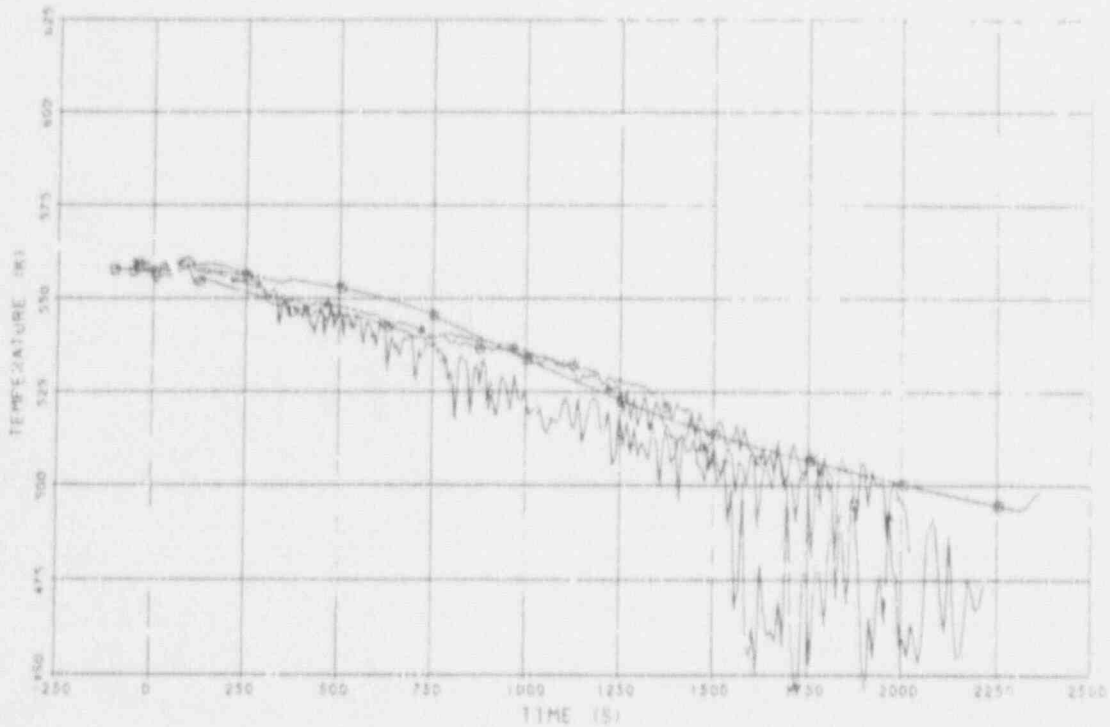
Plot B.32



1987-06-09

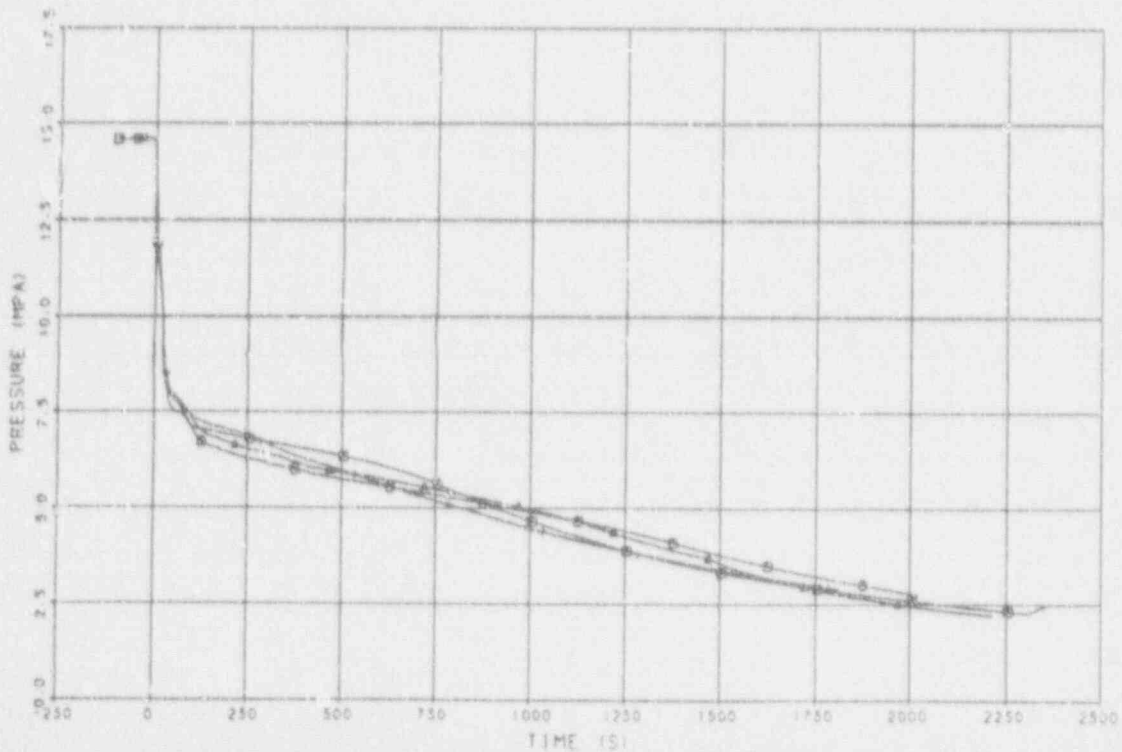
*800 | L | COOL LEG TEMPERATURE | (T-PT-004) EXP.
 | L | COOL LEG TEMPERATURE | (TEMP) 180 | CASE A
 | L | COOL LEG TEMPERATURE | (TEMP) 180 | CASE B
 | L | COOL LEG TEMPERATURE | (TEMP) 180 | CASE C

Plot B.33



*802 | L | COOL LEG PRESSURE | (PE-PC-005) EXP.
 | L | COOL LEG PRESSURE | (P) 120 | CASE A
 | L | COOL LEG PRESSURE | (P) 120 | CASE B
 | L | COOL LEG PRESSURE | (P) 120 | CASE C

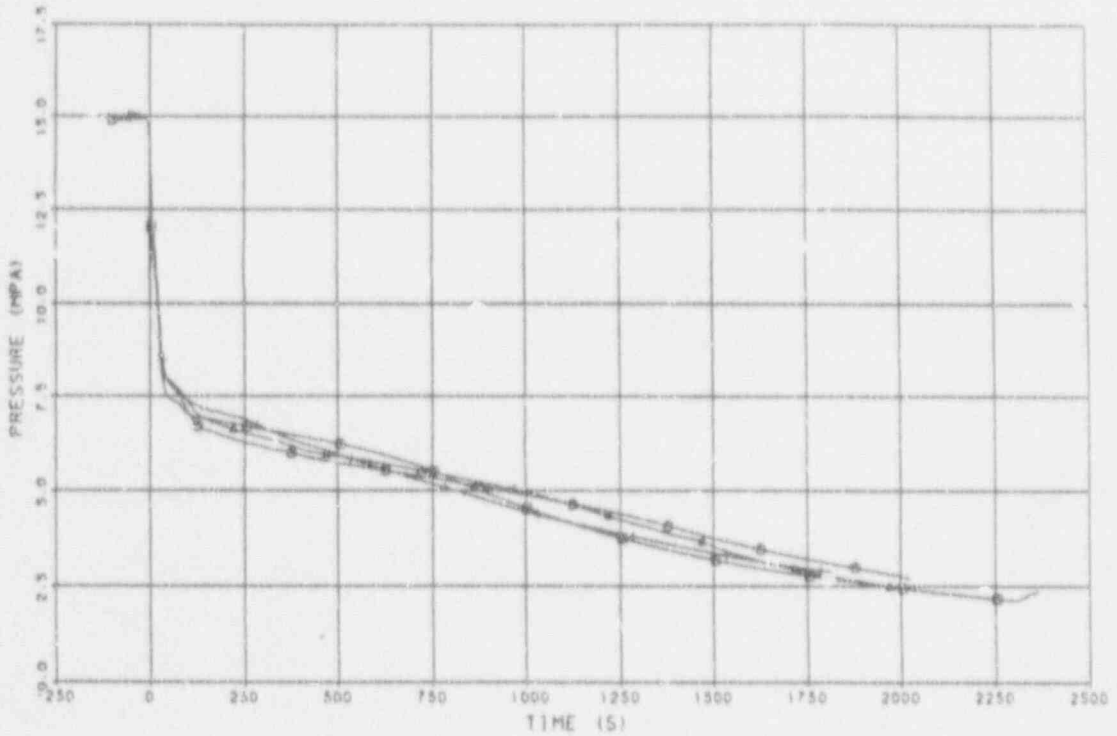
Plot B.34



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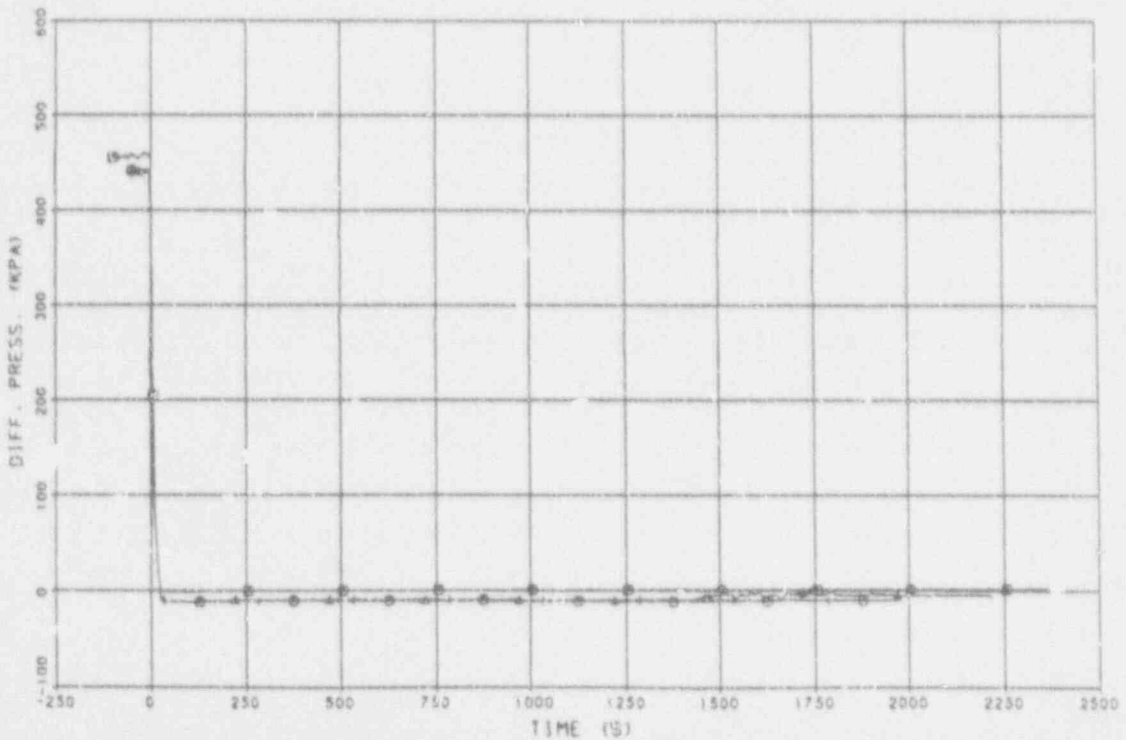
4400 LES PRESSURE IPE-ML-001 EXP.
4401 LES PRESSURE IPE-ML-001 EXP.
4402 LES PRESSURE IPE-ML-001 EXP.
4403 LES PRESSURE IPE-ML-001 EXP.
4404 LES PRESSURE IPE-ML-001 EXP.
4405 LES PRESSURE IPE-ML-001 EXP.
4406 LES PRESSURE IPE-ML-001 EXP.
4407 LES PRESSURE IPE-ML-001 EXP.
4408 LES PRESSURE IPE-ML-001 EXP.
4409 LES PRESSURE IPE-ML-001 EXP.
4410 LES PRESSURE IPE-ML-001 EXP.

Plot B.35



4400 PRESS DIFF ACROSS PUMPS IPE-PC-001 EXP.
4401 PRESS DIFF ACROSS PUMPS ICTRLVAR 9361 CASE A
4402 PRESS DIFF ACROSS PUMPS ICTRLVAR 9361 CASE B
4403 PRESS DIFF ACROSS PUMPS ICTRLVAR 9361 CASE C

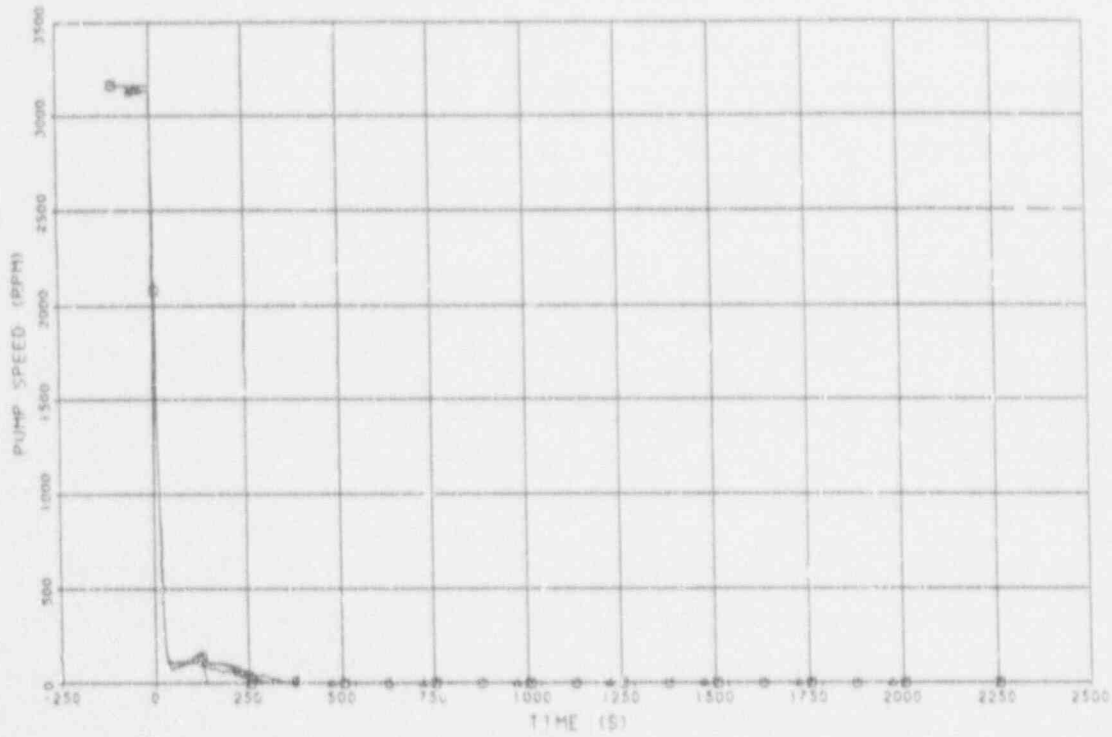
Plot B.36



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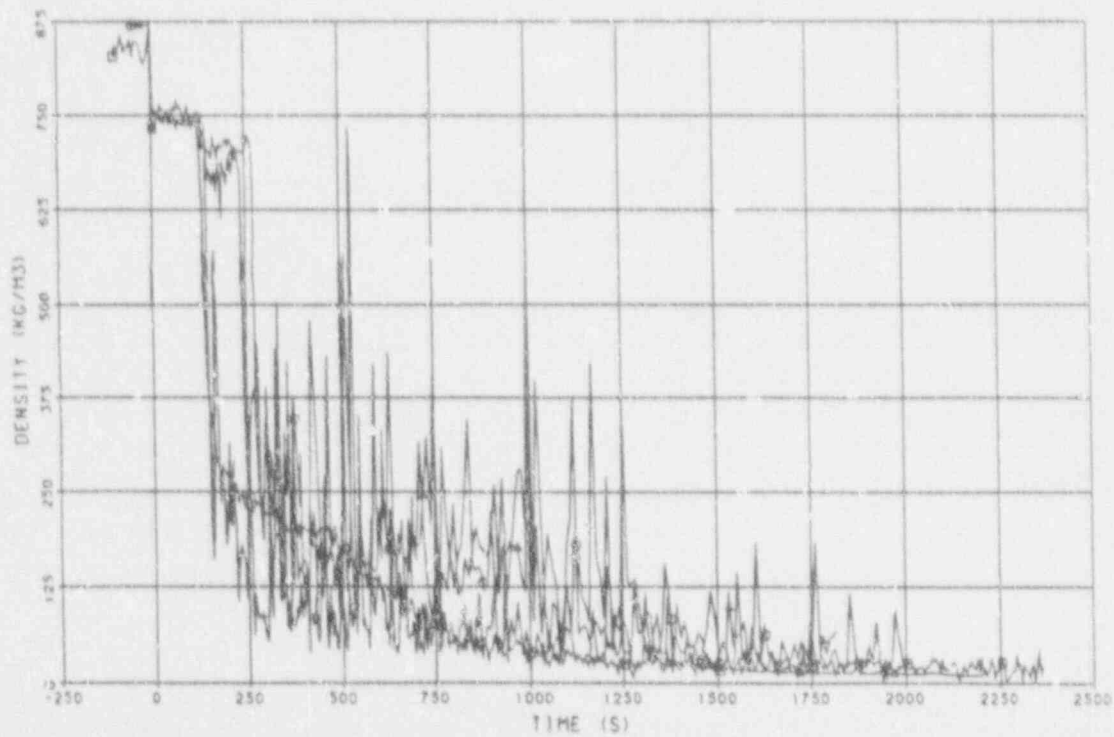
4*08 SPEED OF PUMP | 10PE-PC-0011 EXP
SPEED OF PUMP | 1PUMPVEL 1351 CASE A
SPEED OF PUMP | 1PUMPVEL 1351 CASE B
SPEED OF PUMP | 1PUMPVEL 1351 CASE C

Plot B.37



4*08 BREAK FLUID DENSITY | 10E-PC-502A1 EXP
BREAK FLUID DENSITY | 1RHO #001 CASE A
BREAK FLUID DENSITY | 1RHO #001 CASE B
BREAK FLUID DENSITY | 1RHO #001 CASE C

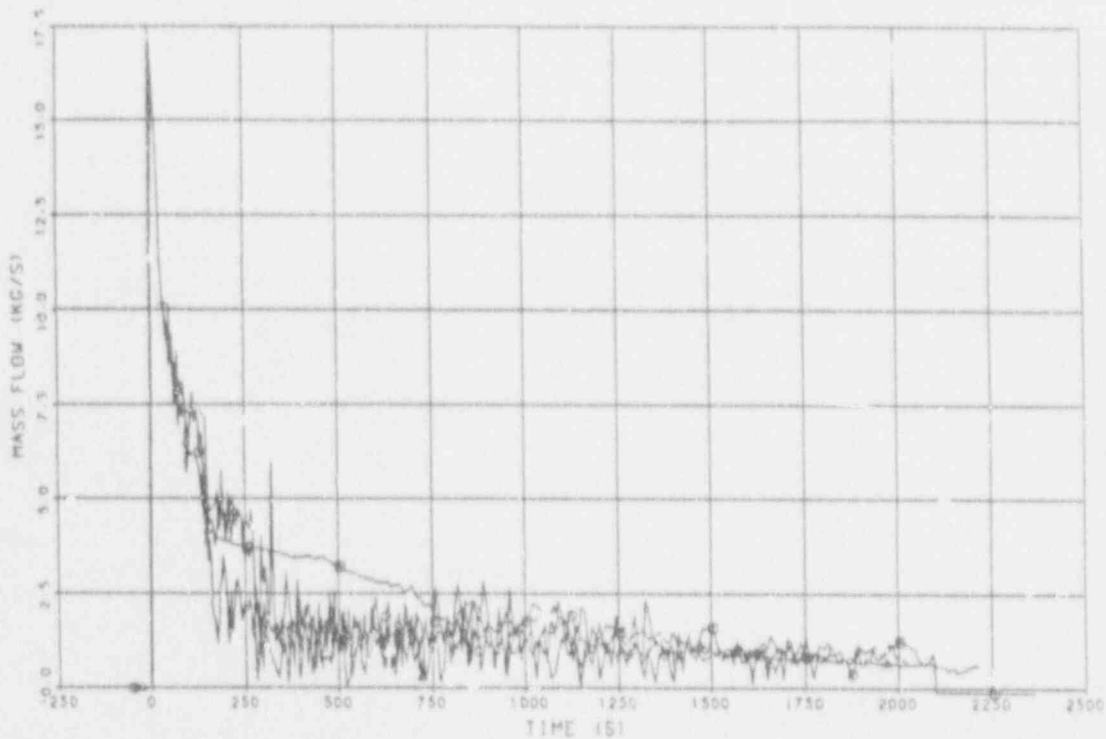
Plot B.38



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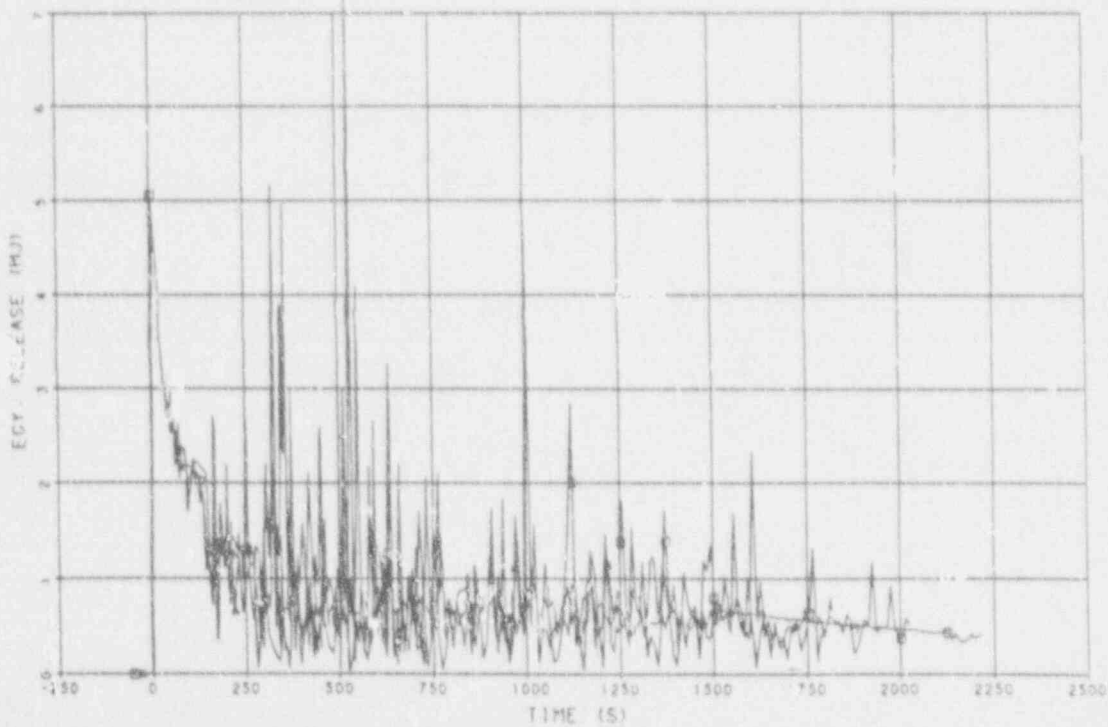
4 000 BREAK MASS FLOW RATE (KG/S) EXP
BREAK MASS FLOW RATE (WLOW) 80S) CASE A
BREAK MASS FLOW RATE (WLOW) 80S) CASE B
BREAK MASS FLOW RATE (WLOW) 80S) CASE C

Plot B.39



100 BREAK ENERGY RELEASE (MW) VAR 840) CASE A
BREAK ENERGY RELEASE (MW) VAR 840) CASE B
BREAK ENERGY RELEASE (MW) VAR 840) CASE C

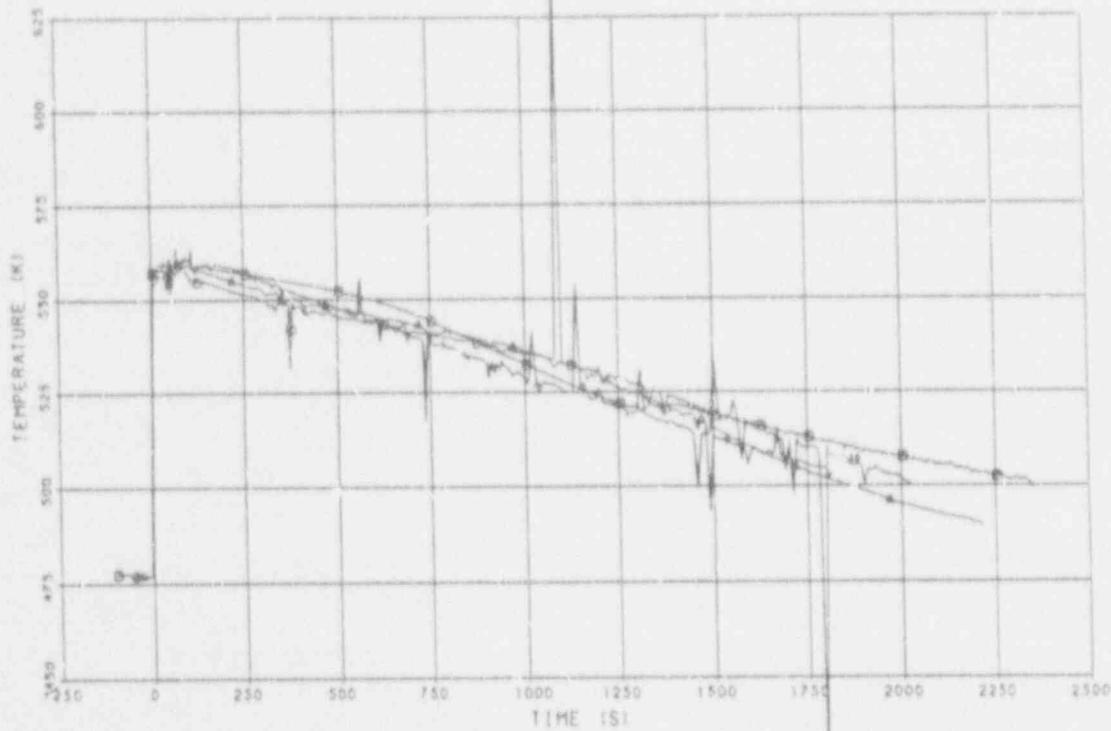
Plot B.40



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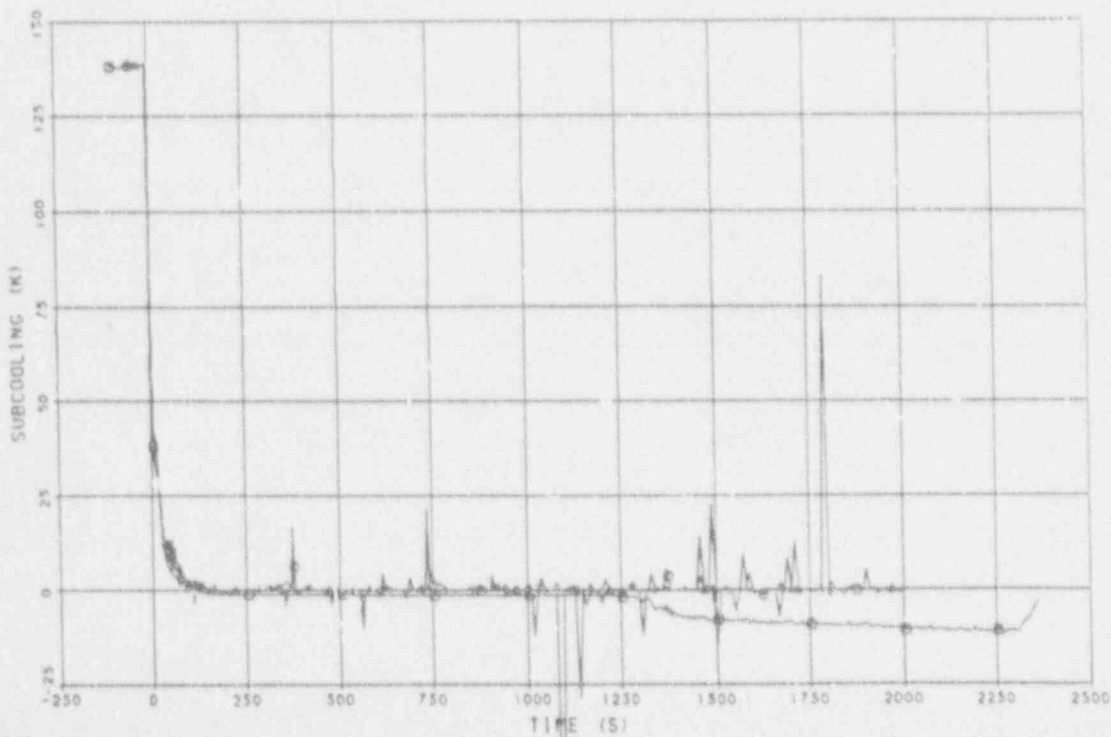
4-408 BREAK INLET TEMPERATURE (T-PC-S01) EXP
 BREAK INLET TEMPERATURE (TEMP 800) CASE A
 BREAK INLET TEMPERATURE (TEMP 800) CASE B
 BREAK INLET TEMPERATURE (TEMP 800) CASE C

Plot B.41



4-408 BREAK INLET SUBC (S1-PC-S10) - T-PC-S01) EXP
 BREAK INLET SUBC (CNTRLVAR 842) CASE A
 BREAK INLET SUBC (CNTRLVAR 842) CASE B
 BREAK INLET SUBC (CNTRLVAR 842) CASE C

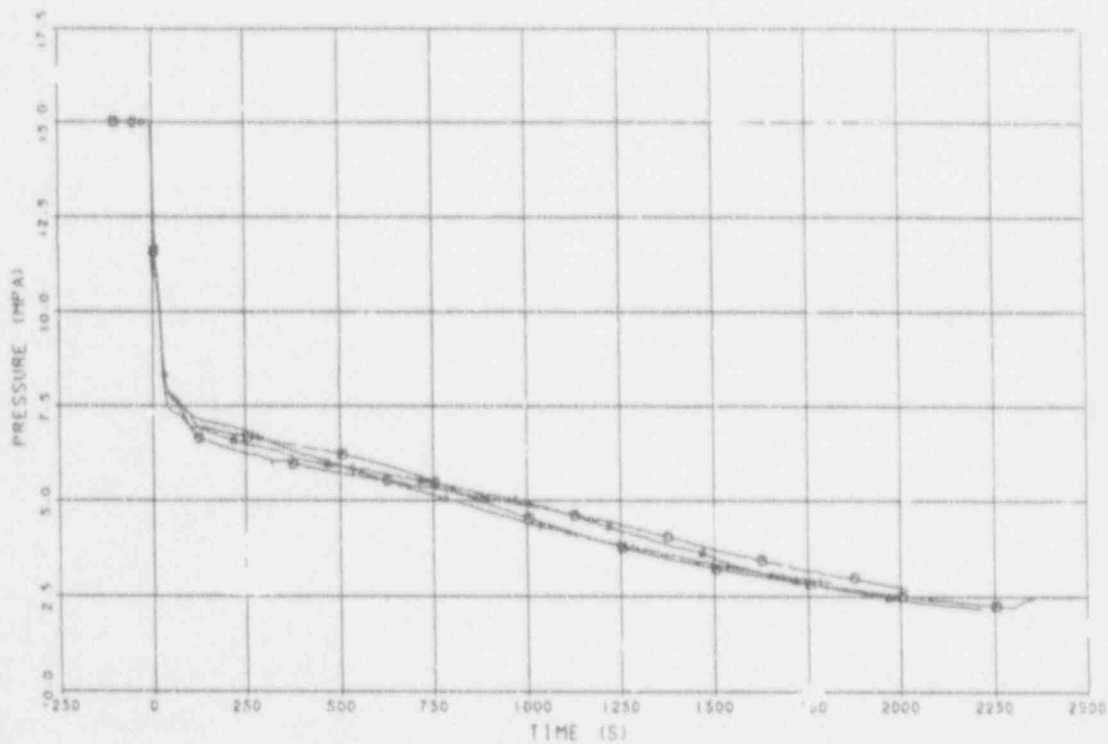
Plot B.42



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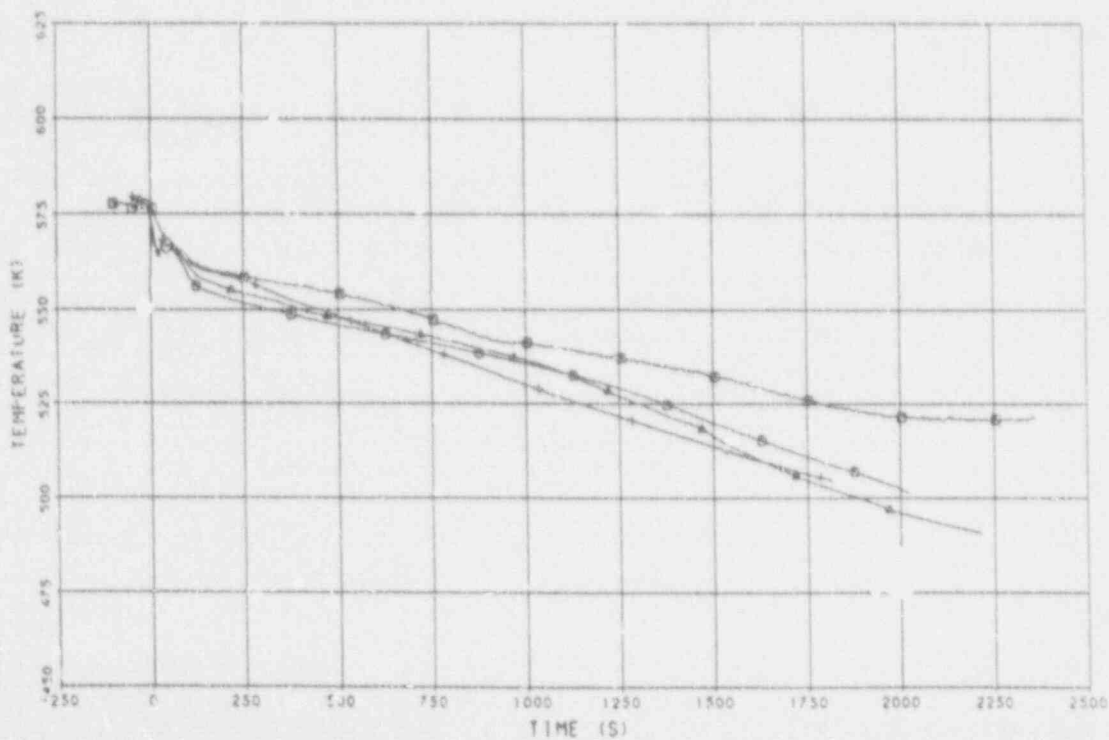
+ #00 BREAK INLET PRESSURE (PE-7C-801) EXP
 + #00 BREAK INLET PRESSURE (P-800) CASE A
 + #00 BREAK INLET PRESSURE (P-800) CASE B
 + #00 BREAK INLET PRESSURE (P-800) CASE C

Plot B.43



+ #00 SC PRI SIDE INLET TEMPERATURE (TS-7C-001) EXP
 + #00 SC PRI SIDE INLET TEMPERATURE (TEMP 115 03) CASE A
 + #00 SC PRI SIDE INLET TEMPERATURE (TEMP 115 03) CASE B
 + #00 SC PRI SIDE INLET TEMPERATURE (TEMP 115 03) CASE C

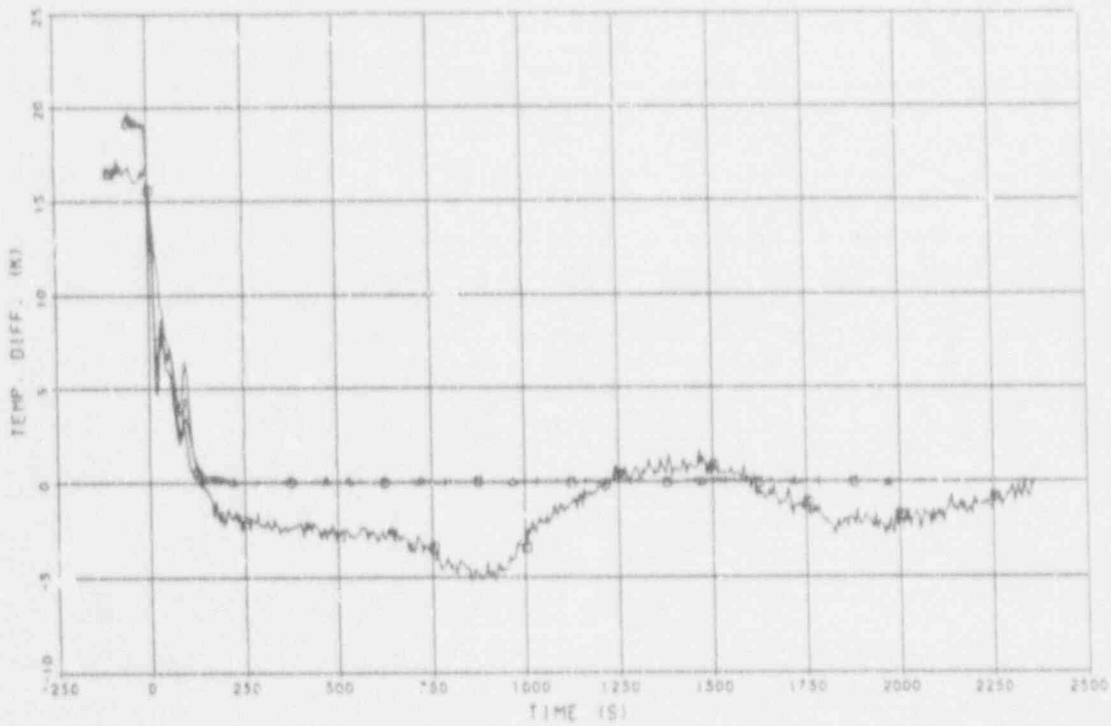
Plot B.44



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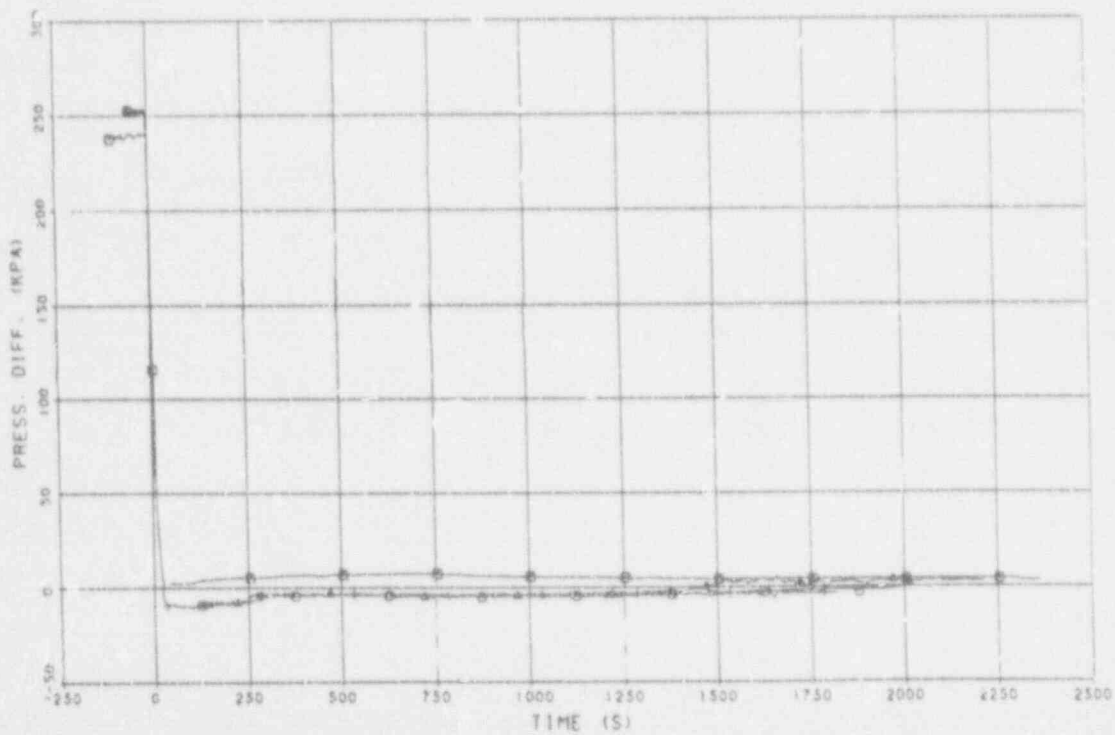
4400 80 PR | TEMP | DIFF | (TE-SC-001 - TE-SC-002) EXP
 80 PR | TEMP | DIFF | (CTRLVAR 945) CASE A
 80 PR | TEMP | DIFF | (CTRLVAR 945) CASE B
 80 PR | TEMP | DIFF | (CTRLVAR 945) CASE C

Plot B.45



4400 80 PR | SIDE | PRESSURE | DIFF | (PDE-PC-002) EXP
 80 PR | SIDE | PRESSURE | DIFF | (CTRLVAR 945) CASE A
 80 PR | SIDE | PRESSURE | DIFF | (CTRLVAR 945) CASE B
 80 PR | SIDE | PRESSURE | DIFF | (CTRLVAR 945) CASE C

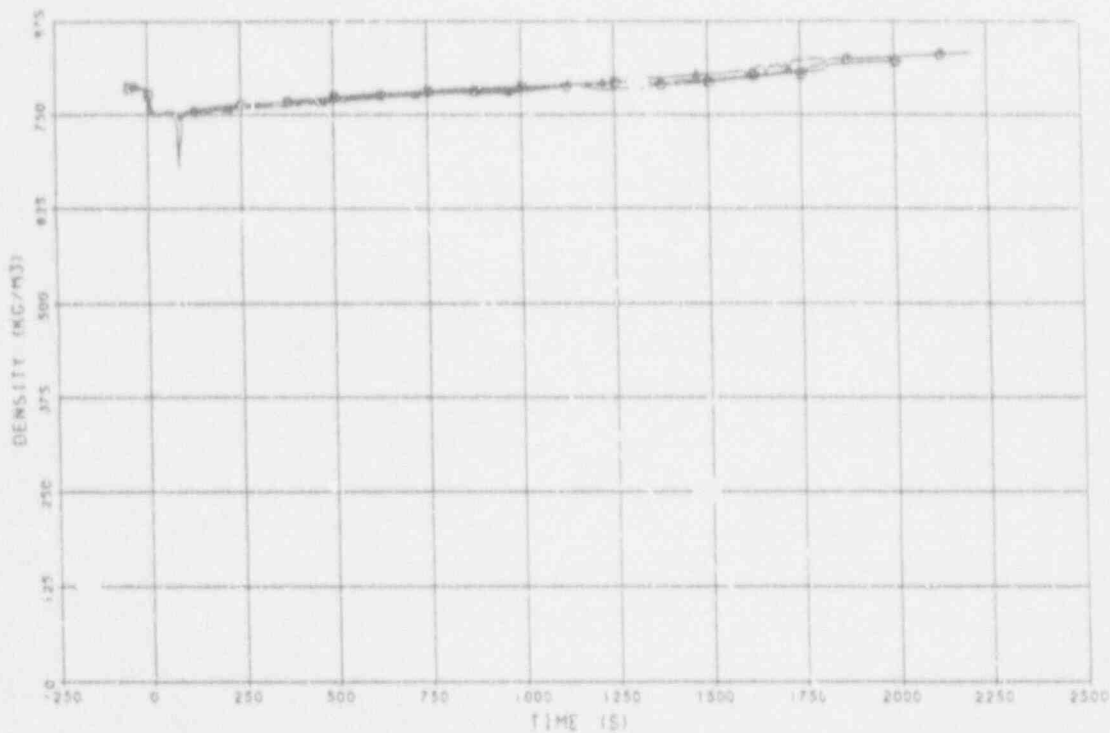
Plot B.46



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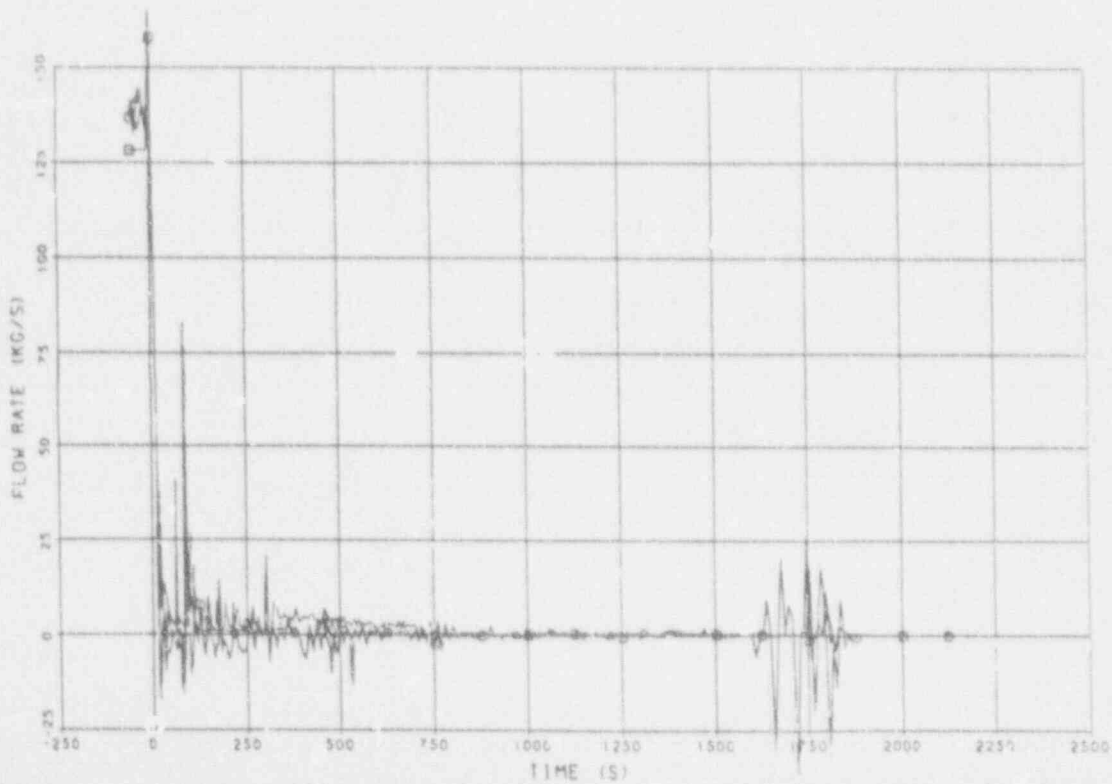
#00 84 FLUID DENSITY (RHO 515 03) CASE A
 84 FLUID DENSITY (RHO 515 03) CASE B
 8C FLUID DENSITY (RHO 515 03) CASE C

Plot B.47



#00 80 MASS FLOW RATE (WFLOWJ 516) CASE A
 80 MASS FLOW RATE (WFLOWJ 516) CASE B
 80 MASS FLOW RATE (WFLOWJ 516) CASE C

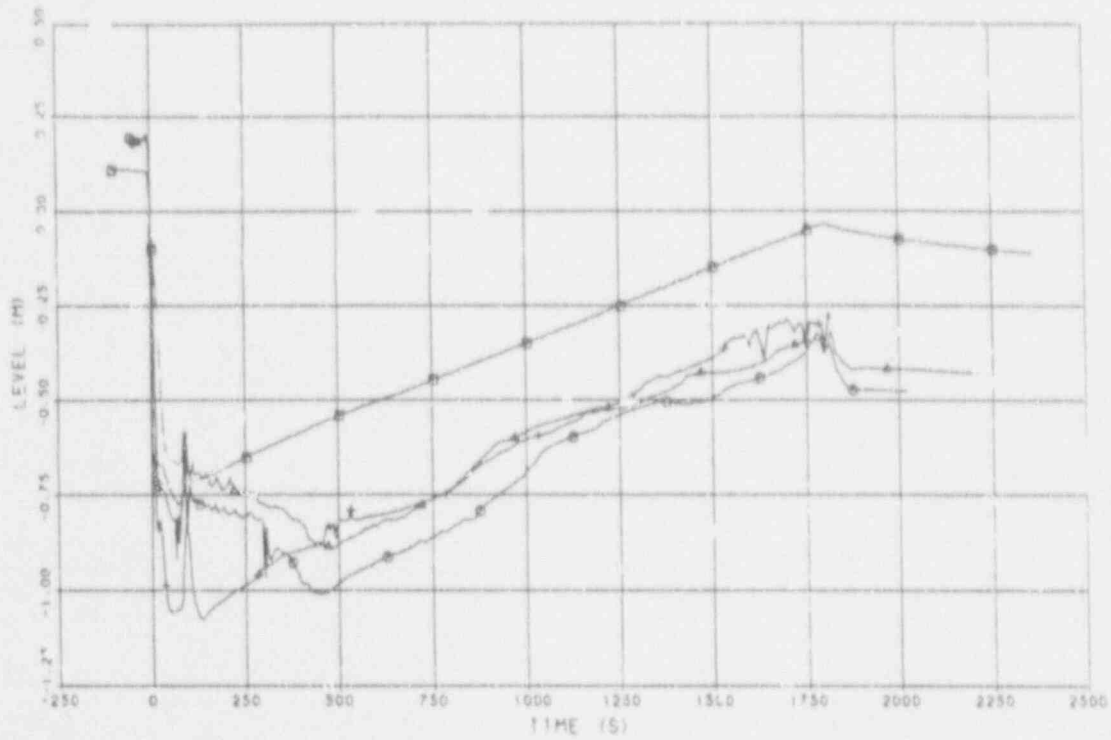
Plot B.48



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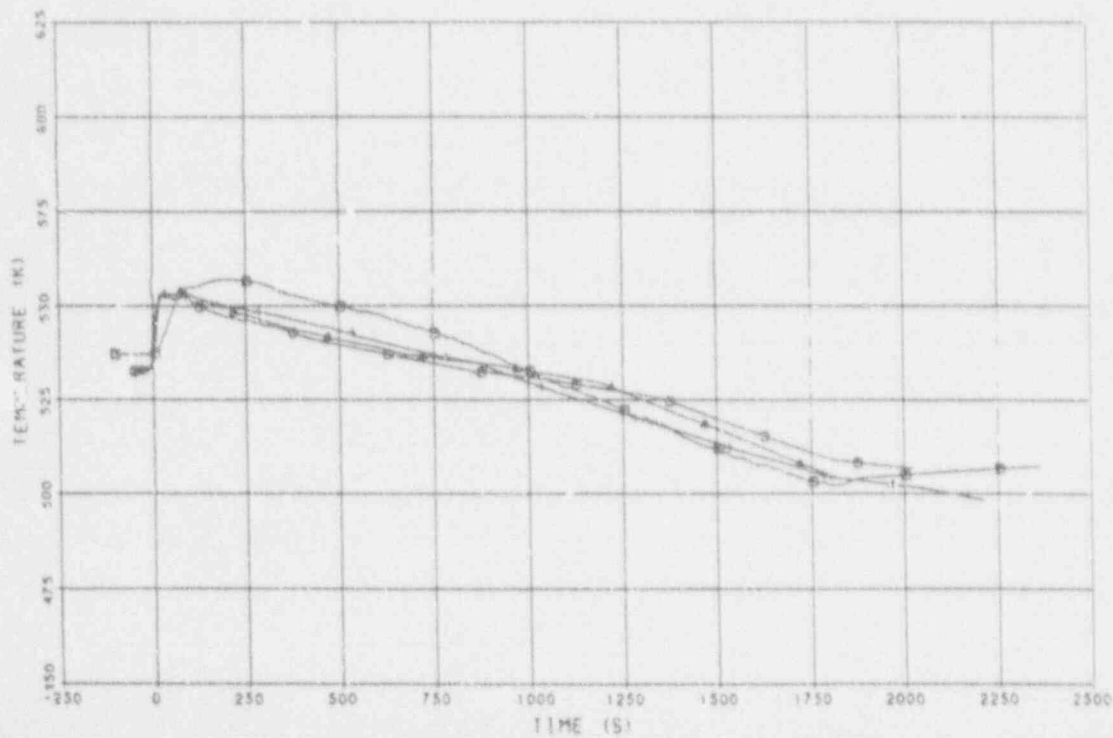
* #008 SC LIQUID LEVEL (LD-P004-D088) EXP
 * SC LIQUID LEVEL (CTRLVAR 949) CASE A
 * SC LIQUID LEVEL (CTRLVAR 949) CASE B
 * SC LIQUID LEVEL (CTRLVAR 949) CASE C

Plot B.49



* #008 SC LIQUID TEMPERATURE (TE SC-003) EXP
 * SC LIQUID TEMPERATURE (TEMP 515 03) CASE A
 * SC LIQUID TEMPERATURE (TEMP 515 03) CASE B
 * SC LIQUID TEMPERATURE (TEMP 515 03) CASE C

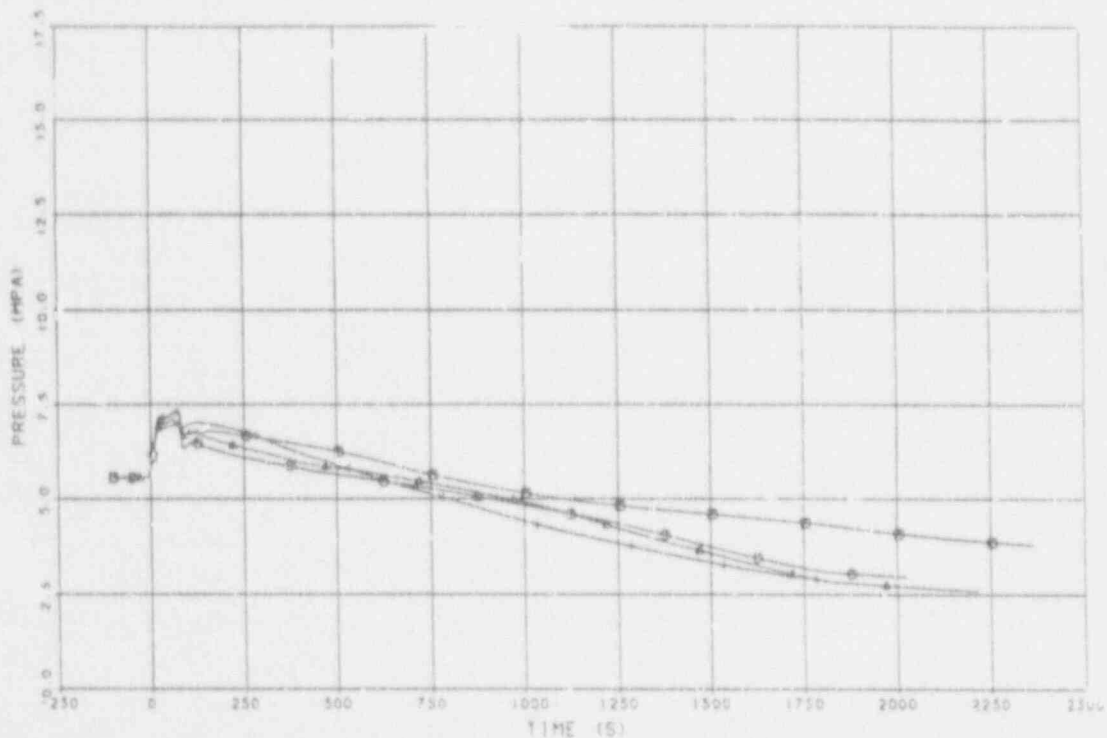
Plot B.50



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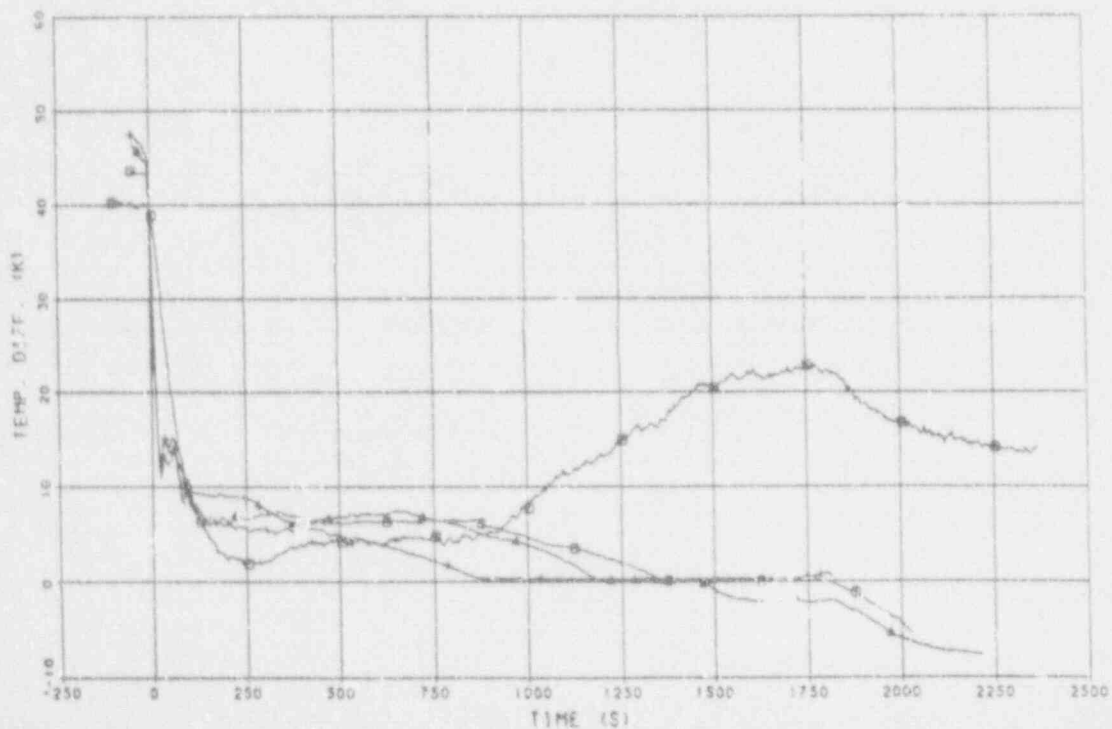
4 6 0 0 SC PRESSURE (PE-101-00) EXP
 4 6 0 0 SC PRESSURE (P 101) CASE A
 4 6 0 0 SC PRESSURE (P 101) CASE B
 4 6 0 0 SC PRESSURE (P 101) CASE C

Plot B.51



4 6 0 0 SC PR1 -500 TEMP DIFF (TE-50-00) - (TE-50-003) EXP
 4 6 0 0 SC PR1 -500 TEMP DIFF (TEMP VAR 51) CASE A
 4 6 0 0 SC PR1 -500 TEMP DIFF (TEMP VAR 52) CASE B
 4 6 0 0 SC PR1 -500 TEMP DIFF (TEMP VAR 53) CASE C

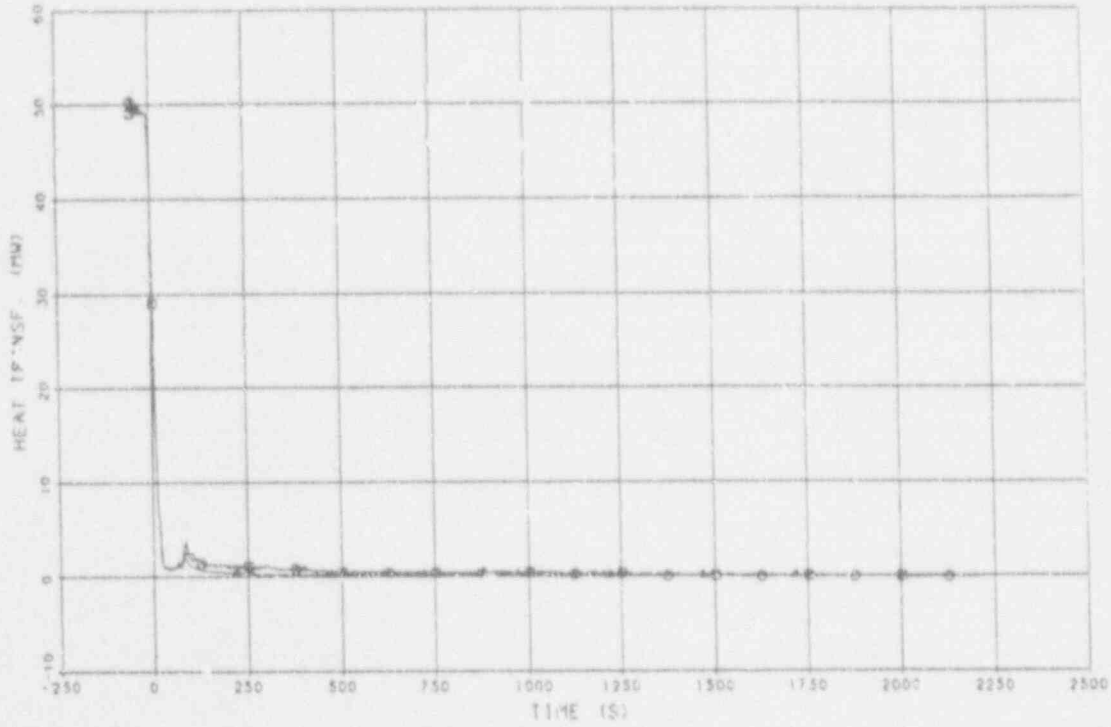
Plot B.52



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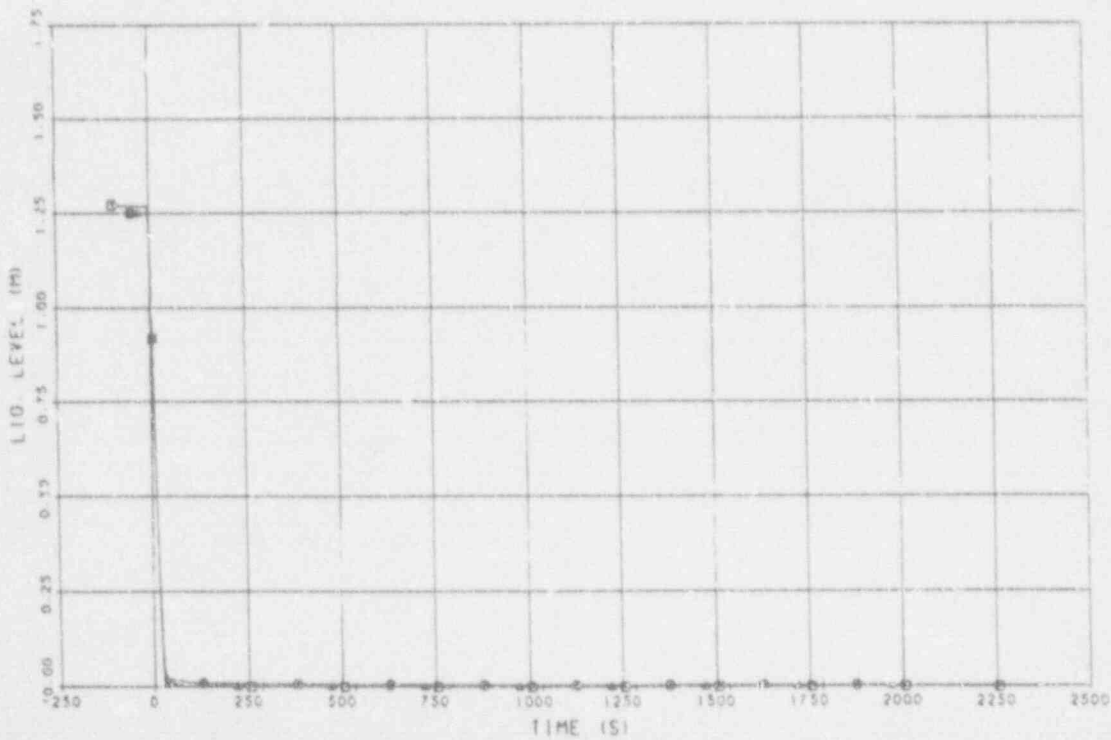
* 00 SC HEAT TRANSFER RATE (CNTRLVAR 953) CASE A
 SC HEAT TRANSFER RATE (CNTRLVAR 953) CASE B
 SC HEAT TRANSFER RATE (CNTRLVAR 953) CASE C

Plot B.53



* 000 PRESSURIZER LIQUID LEVEL (LT-R138-006) EXP
 PRESSURIZER LIQUID LEVEL (CNTRLVAR 954) CASE A
 PRESSURIZER LIQUID LEVEL (CNTRLVAR 954) CASE B
 PRESSURIZER LIQUID LEVEL (CNTRLVAR 954) CASE C

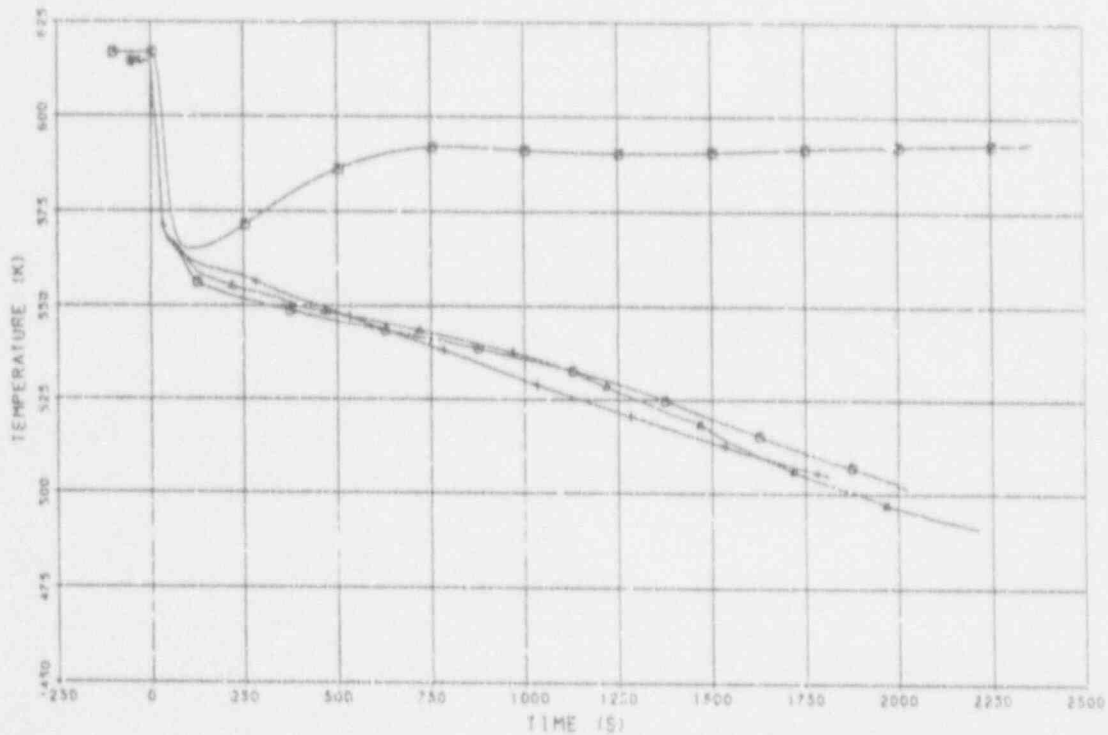
Plot B.54



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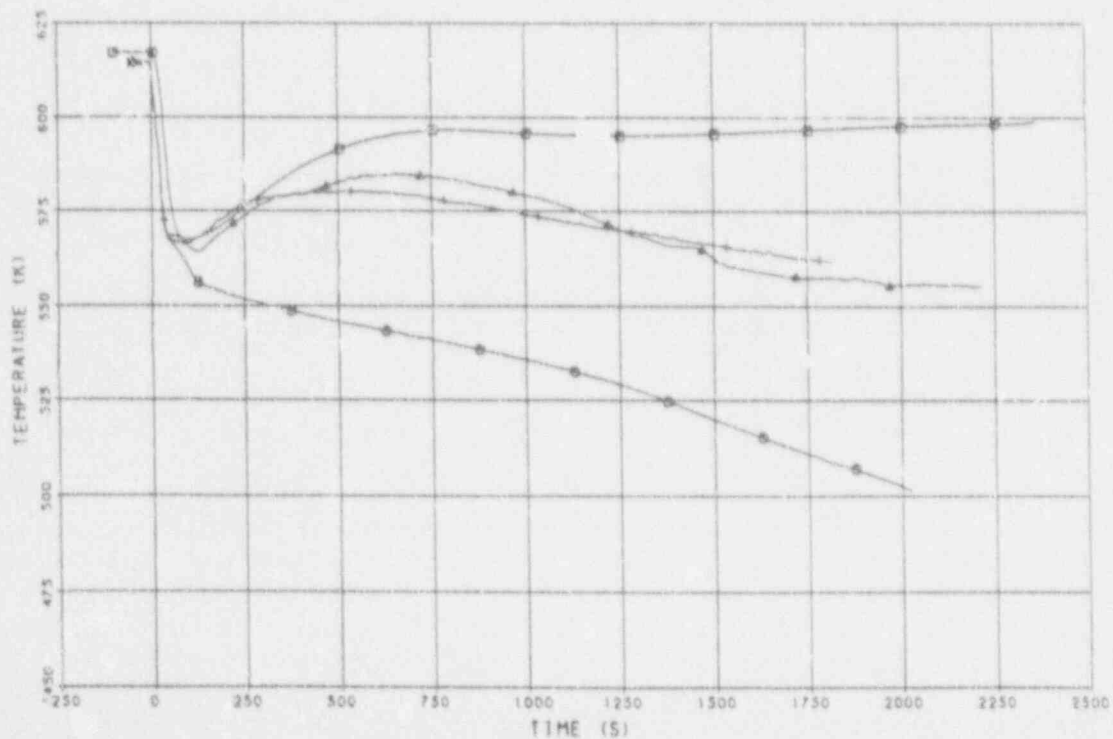
4408 PRESSURE 1228 LIQUID TEM 110-0138-021 EXP
 PRESSURE 1228 LIQUID TEM 110-0138-021 CASE A
 PRESSURE 1228 LIQUID TEM 110-0138-021 CASE B
 PRESSURE 1228 LIQUID TEM 110-0138-021 CASE C

Plot B.55



4408 PRESSURE 1228 LIQUID TEM 110-0138-021 EXP
 PRESSURE 1228 LIQUID TEM 110-0138-021 CASE A
 PRESSURE 1228 LIQUID TEM 110-0138-021 CASE B
 PRESSURE 1228 LIQUID TEM 110-0138-021 CASE C

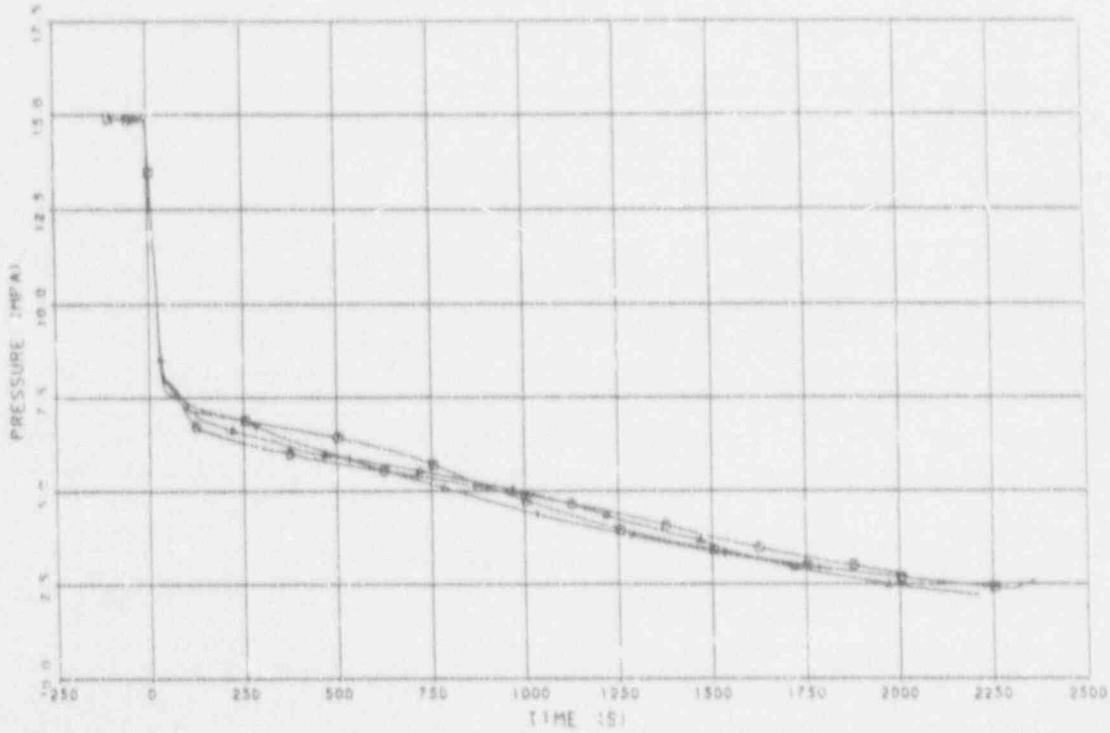
Plot B.56



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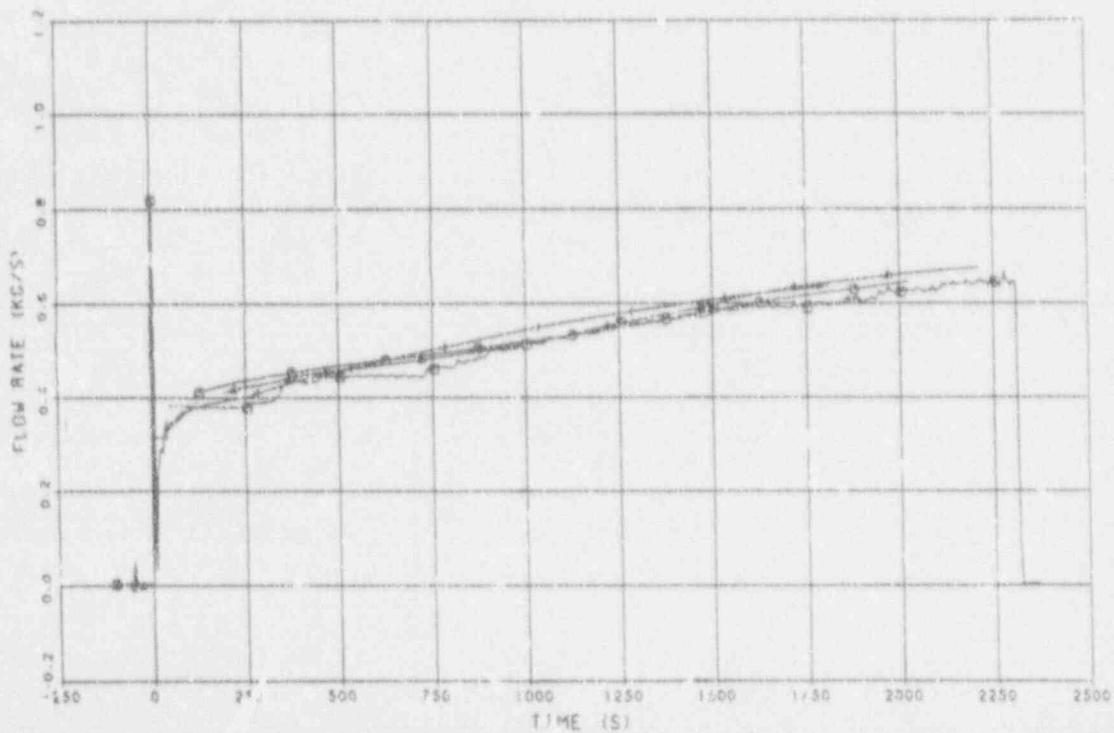
4498 PRESSURIZER PRESSURE (PE-PC-004) EXP.
 PRESSURIZER PRESSURE (P-415-001) CASE A
 PRESSURIZER PRESSURE (P-415-001) CASE B
 PRESSURIZER PRESSURE (P-415-001) CASE C

Plot B.57



4499 HP15 VOLUMETRIC FLOW RATE (FT-F128-104) EXP.
 HP15 VOLUMETRIC FLOW RATE (CTRLVAR 858) CASE A
 HP15 VOLUMETRIC FLOW RATE (CTRLVAR 858) CASE B
 HP15 VOLUMETRIC FLOW RATE (CTRLVAR 858) CASE C

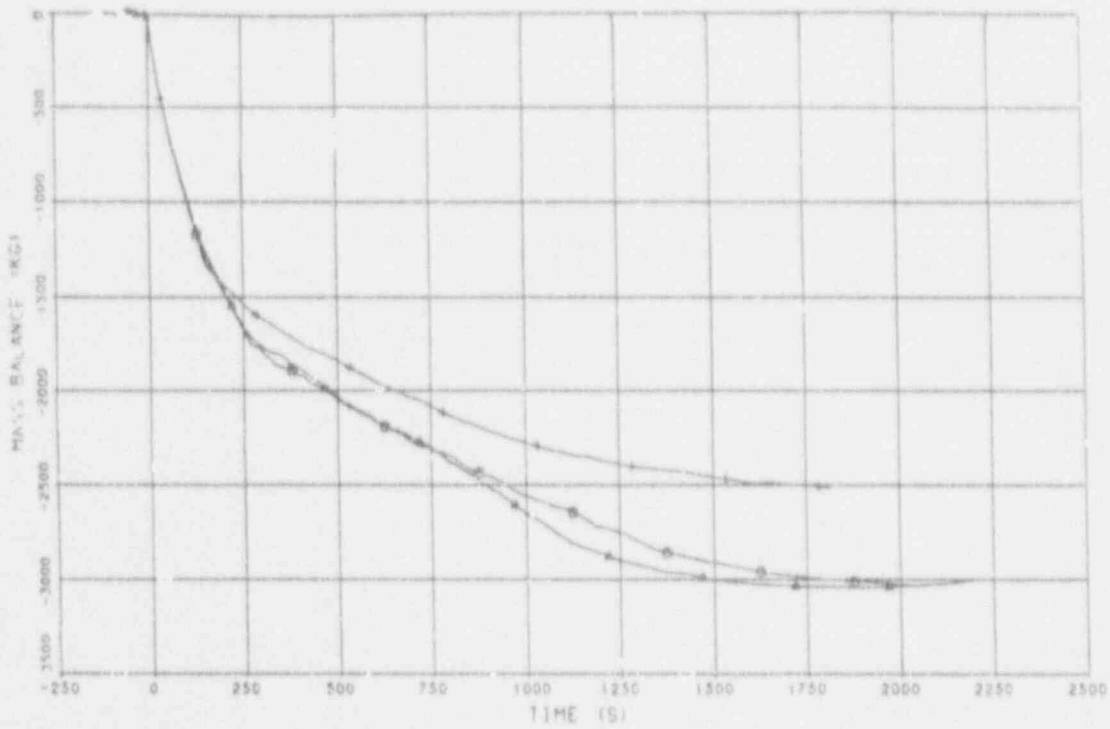
Plot B.58



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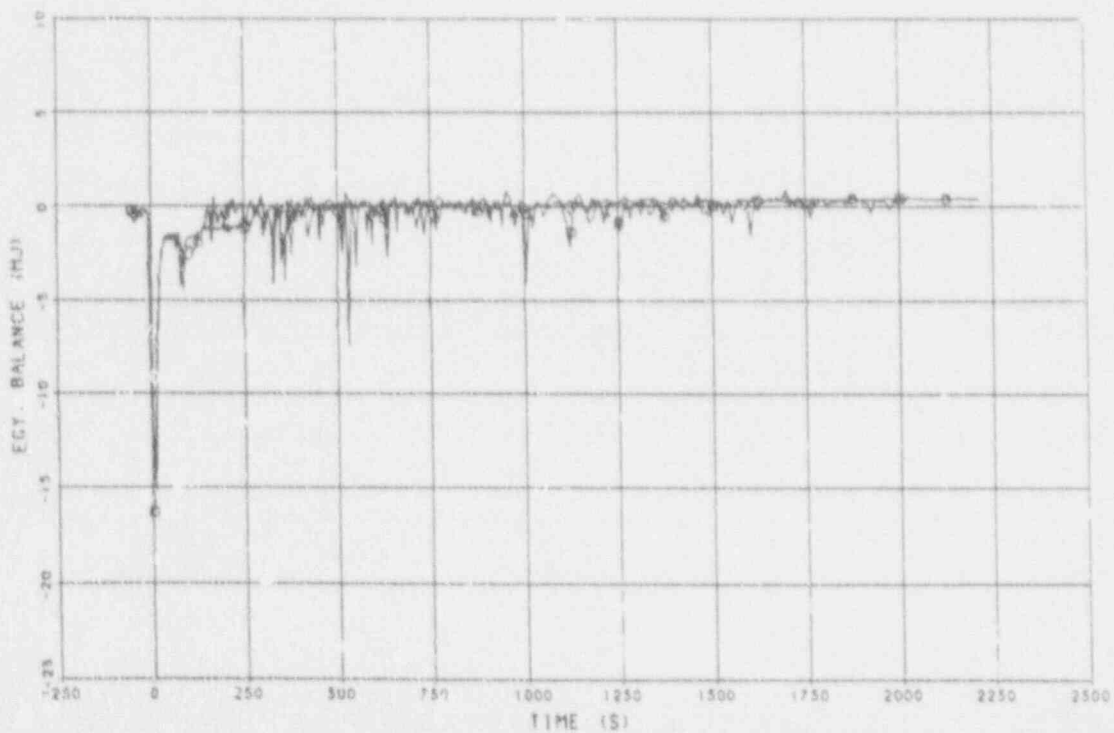
4-B SYSTEM MASS BALANCE (CTRLVAR 958) CASE A
4-B SYSTEM MASS BALANCE (CTRLVAR 959) CASE B
4-B SYSTEM MASS BALANCE (CTRLVAR 959) CASE C

Plot B.59



4-B3 COOLANT ENERGY BALANCE (CTRLVAR 960) CASE A
4-B3 COOLANT ENERGY BALANCE (CTRLVAR 960) CASE B
4-B3 COOLANT ENERGY BALANCE (CTRLVAR 960) CASE C

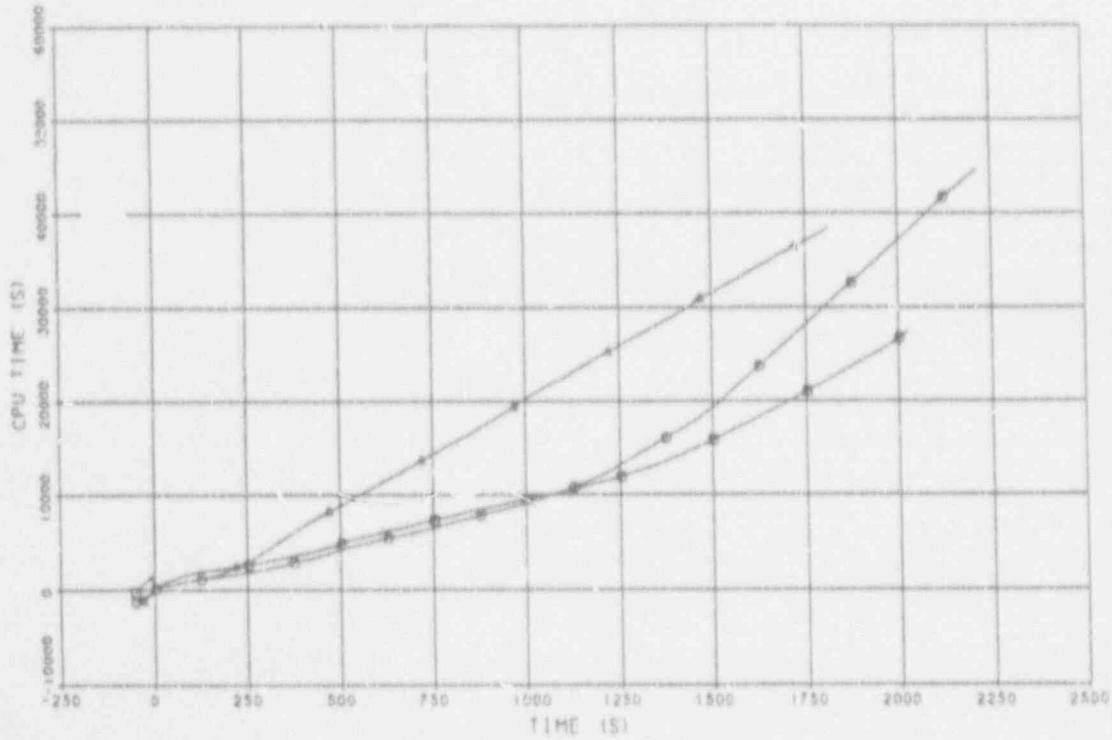
Plot B.60



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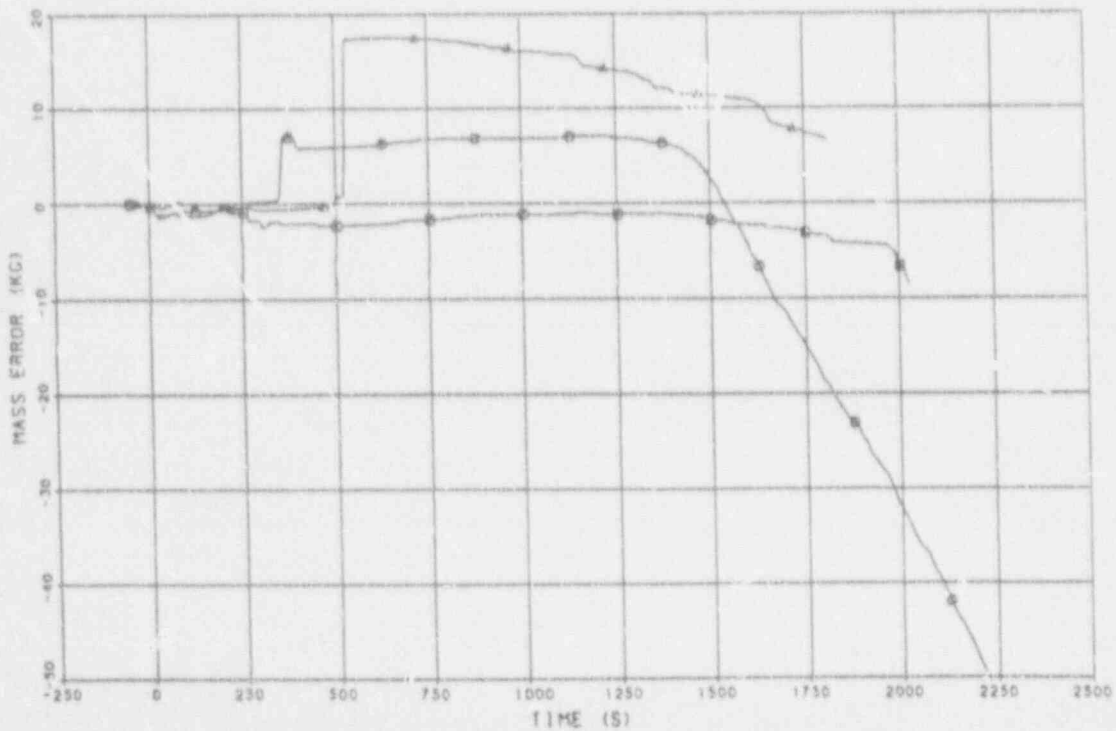
4-90 COMPUTATION CPU TIME (CPU TIME) OF CASE A
 COMPUTATION CPU TIME (CPU TIME) OF CASE B
 COMPUTATION CPU TIME (CPU TIME) OF CASE C

Plot B.61



4-90 COMPUTATION MASS ERROR (EMASS) OF CASE A
 COMPUTATION MASS ERROR (EMASS) OF CASE B
 COMPUTATION MASS ERROR (EMASS) OF CASE C

Plot B.62



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Calculation-to-Experiment Data Uncertainties

CASE A

CALCULATION-TO-EXPERIMENT DATA UNCERTAINTY ANALYSIS FOR HRC/ICAP

FIRST LINE : DIFFERENCE BETWEEN CALCULATED AND (AVERAGED) EXPERIMENTAL DATA AT END OF THE INTERVAL
 SECOND LINE : MEAN DIFFERENCE OVER THE INTERVAL
 THIRD LINE : MEAN SIGMA OVER THE INTERVAL (ROOT MEAN SQUARE OF THE DIFFERENCE)

- CODES -		- - - - TIME INTERVAL - - - -						
CALC.	EXP.	0.0 - 20.00	- 80.00	- 200.0	- 800.0	- 1000.	- 1800.	- 2000.
C 3A - C 3X		-0.46 -6.15 6.22	-8.84 -8.80 6.84	-8.86 -8.25 8.26	-8.44 -7.82 7.85	-8.10 -8.26 8.01	8.08 3.89 4.27	- 520 3.17 3.41
C 4A - C 4X		3.71 11.4 12.2	8.20 3.97 3.18	-8.23 -3.25 3.25	-7.30 -6.51 6.53	1.80 -3.67 4.73	8.76 8.49 8.67	2.42 4.71 4.83
C 5A - C 5X		1.44 7.70 8.85	9.60 1.73 1.08	-8.45 -3.51 4.05	-7.84 -6.73 6.75	1.89 -3.87 4.89	8.08 3.37 8.56	2.85 4.59 4.70
C 6A - C 6X		2.35 9.87 10.4	2.80 1.82 1.88	-8.22 -3.25 3.73	-7.29 -6.42 6.45	2.17 -3.44 4.55	8.37 8.68 8.85	2.79 4.74 4.85
C 8A - C 8X		-8.25 -3.58 3.83	-3.41 -3.78 4.18	-8.47 -8.84 8.85	-8.80 -8.48 8.49	- 280 -6.22 6.04	4.00 3.16 3.49	1.08 2.87 2.81
C 9A - C 9X		- 783 1.49 1.89	5.17 2.11 3.08	-1.78 - 330 1.30	1.76 182 1.85	4.93 4.48 4.65	3.91 4.43 4.61	4.32 3.33 3.26
V 5A - V 5X		-3.45 -4.80 4.52	2.47 -1.04 1.68	10.4 8.83 8.84	11.8 7.69 8.08	-1.85 8.74 10.2	3.28 5.86 5.27	800 2.43 1.85
V 6A - V 6X		-8.15 -3.47 3.61	-2.63 -3.90 4.93	-8.47 -8.48 8.74	-9.91 -9.81 9.82	- 310 -6.28 6.97	3.96 3.12 3.48	1.00 2.81 2.76
V 7A - V 7X		7.87 6.92 8.97	3.76 5.87 6.29	3.03 3.24 3.24	2.60 3.75 3.76	1.77 3.18 3.20	842 1.17 1.21	- 129 -743E-01 938
V 8A - V 8X		-8.39 -4.96 5.01	-8.80 -6.01 6.02	-6.70 -6.16 6.21	-9.88 -9.88 9.89	-12.0 -10.7 11.0	940 -1.30 2.86	-4.41 - 771 1.39
V 9A - V 9X		.119 .366 .308	- .800E-03 .193 .215	- .882 - .388 .472	- 725 - .603 - .685	- .851E-01 - .377 - .481	.288 - .308 - .318	- .392E-01 - .175 - .190
V 2A - V 2X		.167 .294 .412	- .737E-01 - .256 - .271	- .498 - .306 - .388	- .653 - .603 - .605	- .170 - .310 - .408	.399 .393 .402	.185 .283 .281
HL1A - HL1X		82.0 76.5 77.4	96.0 110 113.	-25.1 -7.81 26.2	-55.8 -78.3 87.8	447 280 319	176 266 263.	428 170 175.
HL2A - HL2X		37.1 40.9 41.4	35.3 34.9 35.0	-56.6 -24.4 42.3	-137 -132. 139.	374 218 268	130 233 245.	304 157 160.
HL3A - HL3X		15.5 12.5 13.1	-14.9 -14.3 18.1	-11.8 -8.28 8.80	-42.3 -31.9 33.1	-46.1 -44.8 45.0	-51.4 -60.5 60.6	-47.1 -51.3 51.3
HL4A - HL4X		-1.68 -1.59 - 789	.710 .320 1.81	-4.86 -2.90 3.44	-7.18 -6.40 6.44	-4.09 -4.73 4.87	-10.8 -6.82 7.20	-18.7 -14.4 14.5
HL5A - HL5X		.770E-01 - .228 - .349	- .519E-01 .144 - .172	- .617 - .425 - .464	- .749 - .716 - .717	- .787E-01 - .402 - .483	.281 - .299 - .311	.720E-01 - .189 - .201
CL1A - CL1X		89.7 78.2 78.3	88.0 72.4 72.4	318 229 242.	-185 -34.6 310.	20.4 -65.8 85.8	-40.0 -28.7 41.4	-82.3 -86.2 87.8
CL3A - CL3X		38.1 20.9 21.8	67.3 40.0 41.4	+420. +130. 210.	-256. -321. 329.	- 780 -177. 140.	-180 -86.5 107.	-133. -184. 144.
CL4A - CL4X		.889E-01 .182 - .317	.229E-01 - .348E-01 - .291E-01	- .538E-02 - .657E-02 - .187E-01	- .535E-02 - .106E-01 - .129E-01	- .188E-01 - .150E-01 - .192E-01	- .442E-01 - .346E-01 - .565E-01	- .401 - .861E-01 - .109
CL5A - CL5X		-1.89 -1.90 1.92	-1.10 -1.18 1.19	-1.03 -1.05 1.05	- .838 - .799 - .816	- .215 - .385 - .378	520E-01 - .970E-01 - .131	- .290E-02 - .812E-01 - .862E-01
CL6A - CL6X		-1.88 -2.25 2.10	- .770 -1.18 -1.18	-3.83 -2.44 2.63	-7.14 -8.84 8.78	980 -4.74 8.82	- 680 3.48 3.94	-4.32 -2.05 4.85
CL7A - CL7X		.323 .458 .473	.892E-01 - .298 - .312	- .452 - .273 - .329	- .602 - .583 - .605	.228 - .251 - .367	.428 444 452	.185 - .318 - .326
CL8A - CL8X		.315 - .657 - .870	- .205 - .381 - .397	- .383 - .180 - .259	- .608 - .488 - .470	.322 - .148 - .308	.647 - .558 - .553	.315 - .439 - .445
CL9A - CL9X		2.48 8.57 8.20	-8.86 -8.87 8.99	-10.3 -10.4 10.4	-10.9 -10.3 10.3	-11.9 -11.2 11.4	-11.9 -12.0 12.0	-8.23 -10.9 11.0
CLAA - CLAX		228 147. 181.	-14.4 4.97 86.2	95.7 68.5 81.5	- .443E-02 26.4 39.6	.124 - .182 - .682	823 -1.49 - 2.20	-1.02 - .688 - 1.32

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- 0000 -

- - - - TIME INTERVAL - - - -

CALC. EXP.	0.0 - 30.00	60.00	200.0	500.0	1000.	1500.	2000.
BR1A - BR1X	1.00 20.0 22.0	-21.1 -10.8 12.0	481. 204. 279.	20.7 123. 232.	147. 104. 127.	32.9 85.9 112.	18.0 23.9 37.9
BR2A - BR2X	7.18 8.39 8.55	1.55 2.88 3.32	.227 .734 .870	-1.65 -1.19 1.73	-.387E-01 -.932 1.16	-.281 -.948E-01 .557	-.382 -.125 .236
BR4A - BR4X	-1.99 -1.10 2.83	-1.03 -2.06 2.46	-4.72 -3.42 3.65	-6.65 -6.33 6.66	2.72 -2.80 4.19	8.18 3.83 4.56	-6.09 -4.60 11.2
BR5A - BR5X	4.04 4.54 6.54	2.42 4.98 8.19	.798 1.21 1.41	.847 1.29 2.05	1.13 1.25 1.34	-1.43 3.30 4.53	10.2 10.9 14.8
BR6A - BR6X	.276 .811 .528	.148 .321 .340	-.288 -.271 .268	-.602 -.479 .481	.307 -.148 .302	.481 .509 .614	.218 .255 .365
SP1A - SP1X	-8.49 -7.46 7.47	-2.13 -3.48 4.02	-6.21 -5.18 8.20	-6.12 -7.67 7.63	-4.95 -6.33 6.48	-12.7 -8.47 8.75	-19.1 -15.2 18.3
SP2A - SP2X	-5.41 -2.32 2.42	.113 -.688 1.91	2.29 1.85 1.90	2.62 2.31 2.33	3.29 3.65 3.74	-.455 .241 1.17	2.32 1.17 1.86
SP3A - SP3X	-2.66 8.88 10.7	-11.8 -10.7 10.9	-13.7 -12.6 12.9	-10.3 -10.8 11.0	-10.1 -11.0 11.1	-6.59 -9.12 9.17	-4.18 -6.17 8.21
SS3A - SS3X	-.309 -.243 -.293	-.128 -.175 -.180	-.123 -.879E-01 -.353E-01	-.441 -.301 .323	-.341 -.405 .405	-.348 -.306 -.307	-.403 -.358 -.360
SS4A - SS4X	12.8 5.22 6.99	1.15 8.04 6.47	-10.0 -8.12 6.70	-10.1 -10.3 10.3	-1.84 -2.56 7.98	7.83 4.40 8.30	2.01 6.35 6.67
SS5A - SS5X	-.185E-01 -.179 .192	-.869E-01 -.879E-01 -.104	-.527 -.369 .386	-.608 -.603 .604	-.319 -.414 .426	-.849 -.514 -.539	-1.12 -1.10 1.11
S 1A - S 1X	-21.0 -12.7 13.7	-3.28 -8.62 10.4	3.83 8.38 1.98	1.62 2.67 2.74	-3.34 1.27 1.87	-20.8 -12.7 13.8	-20.9 -21.6 21.6
P 1A - P 1X	-.821E-01 -.602E-01 -.649E-01	-.126E-01 -.284E-01 -.376E-01	-.679E-02 -.881E-02 -.897E-02	-.486E-02 -.589E-02 -.592E-02	-.371E-02 -.474E-02 -.474E-02	-.368E-02 -.391E-02 -.392E-02	-.314E-02 -.315E-02 -.316E-02
P 2A - P 2X	-21.2 -12.3 13.4	-2.93 -12.8 15.5	-14.7 -9.35 9.82	-40.0 -28.1 29.0	-55.8 -49.6 49.8	-70.7 -61.8 61.9	-89.7 -80.2 80.4
P 3A - P 3X	-20.9 -13.5 14.2	-4.60 -13.1 15.3	-18.7 -12.3 12.9	-45.3 -33.1 34.0	-60.0 -54.3 54.5	-75.8 -66.6 66.8	-94.8 -85.5 85.7
P 4A - P 4X	-.210E+01 -.185 .181	-.118E+01 -.210 .228	-.847 -.357 .402	-.695 -.649 .650	-.116 -.343 .434	.342 .350 .359	.796E+01 .220 .231
EC1A - EC1X	-.315E-01 -.300E-01 .168	-.161E-01 -.144E-01 -.766E-01	.488E-01 -.291E-01 -.341E-01	-.238E-01 -.367E-01 -.401E-01	.817E-02 -.261E-01 -.282E-01	-.109E-02 -.870E-03 -.452E-02	-.222E-01 -.158E-01 -.181E-01

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Case B

CALCULATION-TO-EXPERIMENT DATA UNCERTAINTY ANALYSIS FOR HRC 10AP

FIRST LINE : DIFFERENCE BETWEEN CALCULATED AND (AVERAGED) EXPERIMENTAL DATA AT END OF THE INTERVAL
 SECOND LINE : MEAN DIFFERENCE OVER THE INTERVAL
 THIRD LINE : MEAN SIGMA OVER THE INTERVAL (ROOT MEAN SQUARE OF THE DIFFERENCE)

- CODES -		- - - TIME INTERVAL - - -						
CALC.	EXP.	0.0 - 20.00	- 60.00	- 200.0	- 600.0	- 1000.	- 1800.	- 2000.
C 36 - C 3X		-3.95 -4.56 4.72	-3.64 -4.86 4.90	-4.03 -2.79 2.91	-6.49 -5.66 5.64	1.67 -3.63 4.43	1.67 2.75 2.60	-6.04 -2.22 2.88
C 48 - C 4X		4.38 11.5 13.3	2.29 4.45 4.61	-2.71 -1.768 1.88	-5.21 -4.31 4.41	2.71 -1.10 3.58	2.77 3.98 3.99	-2.79 -1.04 2.05
C 58 - C 5X		2.78 9.09 11.2	1.78 3.01 3.14	-2.90 -1.12 1.96	-5.54 -4.62 4.62	-2.52 -2.20 3.60	2.68 3.85 3.86	-3.79 -1.20 2.15
C 68 - C 6X		2.97 10.6 12.7	1.79 3.03 3.12	-2.67 -1.767 1.79	-5.25 -4.22 4.32	3.00 -1.86 3.28	2.97 4.16 4.17	-3.60 -1.09 2.08
C 88 - C 8X		-4.72 -2.19 2.96	-1.65 -2.61 3.01	-6.88 -4.14 4.38	-7.67 -7.27 7.32	640 -4.63 6.37	660 1.62 1.67	-6.38 -3.15 3.56
C AB - C AX		-2.18 858 1.70	2.68 1.28 3.60	+1.51 -327 1.30	1.72 -213E-01 1.24	4.04 4.22 4.31	1.95 3.17 3.27	-218 -362 -614
V 58 - V 5X		-1.50 -2.18 2.20	4.04 4.96 1.30	13.0 8.65 11.8	13.9 10.0 10.3	-1.04 8.31 11.8	1.47 1.14 1.32	-6.01 -3.25 3.77
V 68 - V 6X		-4.93 -1.87 2.65	-1.15 -2.70 3.90	-6.88 -3.98 4.30	-7.95 -7.29 7.34	610 -4.68 5.40	360 1.60 1.63	-8.46 -3.20 3.61
V 78 - V 7X		7.35 8.71 6.05	3.77 5.61 6.95	3.05 3.25 3.26	2.81 2.75 2.76	1.76 2.18 2.20	644 1.17 1.21	-118 -798E-01 333
V 88 - V 8X		-2.75 -2.72 0.79	-4.03 -3.98 4.03	-4.37 -3.65 3.71	-6.97 -7.28 7.55	-3.62 -6.89 9.21	-1.50 -1.58 1.87	-6.76 -3.67 4.06
V 98 - V 9X		266 405 424	172 300 314	-325 -132 218	-550 -473 480	-154 -240 333	627E-01 206 209	-280 -143 173
V AB - V AX		313 437 451	246 363 373	-239 -504E-01 177	-478 -394 403	238 -173 289	194 291 292	-186 -359E-01 101
HL18 - HL1X		60.3 72.9 73.6	107. 108. 111.	-26.2 -3.26 30.5	-51.8 -91.0 94.8	295. 274. 309.	418. 198. 212.	401. 385. 385.
HL28 - HL2X		58.2 41.9 42.4	36.4 35.9 36.1	-69.6 -7.16 59.1	-142. -153. 155.	257. 209. 256.	264. 175. 160.	260. 257. 257.
HL38 - HL3X		10.1 10.5 11.6	-14.9 -13.1 17.4	-16.0 -9.88 10.1	-43.1 -35.2 35.9	-47.2 -44.6 44.7	-49.5 -50.6 50.6	-52.3 -52.1 62.1
HL48 - HL4X		-690 1.92 2.52	2.25 1.59 2.25	-2.25 -394 1.67	-5.29 -4.18 4.32	-3.22 -3.13 3.38	-14.3 -8.34 9.06	-25.1 -20.3 20.5
HL58 - HL5X		224 272 367	121 282 280	-360 -169 239	-575 -506 612	149 -269 353	753E-01 198 200	-247 -128 188
CL'8 - CL1X		65.3 72.0 72.1	64.8 69.5 69.6	386. 215 226.	-185. -84.8 185.	21.3 -60.6 94.8	-77.2 -70.0 76.3	-109 -91.0 91.2
CL28 - CL2X		29.2 21.9 22.8	68.4 41.1 42.4	-421. -78.6 181.	-246. -295. 304.	-42.5 -109. 104.	-183. -132. 137.	-135. -144. 145.
CL38 - CL3X		602E-01 170 182	-240E-01 -283E-01 308E-01	-198E-01 -675E-03 -234E-01	-880E-02 -139E-01 -150E-01	-821E-02 -127E-01 -167E-01	-476 -602E-01 111	-346 351 396
CL48 - CL4X		-1.59 -1.90 1.91	-1.10 -1.18 1.19	-1.72 -1.04 1.04	-583 -795 809	-197 -359 382	-716E-01 -640E-01 111	-185 -746E-01 985E-01
CL58 - CL5X		240 273 393	860 408 422	-1.07 -862 896	-6.06 -4.13 4.46	1.91 -3.22 4.24	-4.22 682E-01 2.63	-43.5 -33.1 35.9
CL78 - CL7X		373 504 614	272 405 415	-186 -166E-01 170	-427 -354 363	297 -114 260	219 -341 343	-137 -396E-01 969E-01
CL88 - CL8X		462 600 610	378 494 502	-106 -781E-01 187	-331 -259 271	400 -110E-01 236	344 453 455	-160E-02 122 155
CL98 - CL9X		-2.80 1.92 11.8	-9.78 -8.75 9.03	-9.75 -10.2 10.3	-10.8 -10.1 10.1	-12.4 -11.2 11.2	-5.12 -11.3 11.4	-6.27 -5.70 5.89
CLAB - CLAX		158. 129. 143.	-12.4 11.8 68.1	64.2 86.3 80.4	-443E-02 15.7 29.2	124 -192 891	1.47 -1.32 2.20	-2.74 -616E-02 1.18

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- CODES -		- - - - TIME INTERVAL - - - -						
CAIC	EXP.	0 0 - 20 00	- 60 00	- 200 0	- 600 0	- 1000	- 1600	- 2000
BR1B - BR1X		-2.40 17.4 20.7	-24.6 -14.5 16.1	400. 184. 265.	-14.4 73.8 176.	665. 110. 136.	6.23 66.0 91.1	4.61 -6.67 8.96
BR2B - BR2X		7.06 7.98 8.08	689 2.02 3.21	665 689 773	-2.81 -1.41 1.88	-380 -667 1.27	-625 -167 388	-194 -234 290
BR4B - BR4X		- .000E-01 - .775E-01 .511	.820 - .838E-01 1.64	-2.18 - .552 1.67	-4.44 -4.08 4.21	2.02 -1.64 3.16	-3.68 4.41 16.2	-12.9 -6.65 8.97
BR5B - BR5X		3.20 3.74 3.69	2.35 3.96 4.30	.774 858 1.16	.988 1.31 1.44	2.49 1.82 1.68	7.91 1.20 14.6	10.3 6.66 8.66
BR6B - BR6X		.423 .872 .663	.343 .442 .450	-.141 - .346E-01 .177	-.324 -.264 .275	.367 - .775E-02 .228	.269 .395 .387	-.105 - .255E-01 - .895E-01
SP1B - SP1X		-7.66 -6.36 6.51	- .570 -2.07 2.89	-3.61 -2.67 2.00	-6.10 -3.40 6.47	-4.14 -4.73 4.85	-16.1 -10.0 10.6	-28.6 -21.1 21.2
SP2B - SP2X		-6.08 -2.61 3.13	- .985 -1.09 1.95	2.16 1.07 1.43	2.73 2.29 2.31	3.29 3.64 3.73	- .442 1.241 1.17	2.37 1.20 1.68
SP3B - SP3X		-4.88 2.48 8.26	-11.8 -10.6 10.8	-13.1 -12.6 12.6	-10.3 -10.2 10.3	-9.63 -10.9 11.0	-2.86 -7.82 6.01	-1.06 -1.56 1.85
SS3B - SS3X		- .269 - .237 .279	- .102 - .103 - .109	- .818E-01 - .162E-01 - .308E-01	-.340 - .197 - .218	- .234 - .297 - .299	- .276 - .258 - .269	- .344 - .316 - .317
SS4B - SS4X		12.6 6.18 7.73	-1.21 4.65 6.31	-7.88 -4.50 4.92	-8.76 -9.01 9.02	- .220 -6.98 6.64	6.19 4.04 4.33	-2.66 2.39 3.61
SS5B - SS5X		.991E-01 - .835E-01 .118	.311 .265 .276	-.263 - .876E-01 - .172	-.443 - .401 - .406	- .243 - .281 - .290	-1.02 - .600 - .647	-1.38 -1.02 -1.53
S 1B - S 1X		-20.2 -11.6 13.0	-.626 -6.72 9.12	3.98 1.83 2.22	2.33 3.62 3.76	-4.24 1.08 2.32	-21.4 -13.9 14.7	-22.6 -23.6 23.5
P 1B - P 1X		.706E-01 .670E-01 .619E-01	.911E-03 .178E-01 .314E-01	-.616E-03 .672E-05 - .47E-03	-.402E-03 - .285E-03 .344E-03	-.476E-03 - .896E-04 .278E-03	.433E-03 - .197E-03 - .265E-03	.875E-03 - .466E-03 - .636E-03
P 2B - P 2X		-20.1 -11.6 12.9	-1.36 -11.6 14.7	-12.1 -5.83 7.62	-37.9 -26.8 27.0	-64.7 -48.0 48.7	-74.1 -63.3 63.6	-86.1 -86.1 86.3
P 3B - P 3X		-19.8 -12.9 13.5	- .800E-01 -11.2 14.4	-1.85 -2.41 2.62	-8.54 -4.85 6.56	-16.8 -12.6 12.7	-33.3 -24.3 24.8	-41.7 -36.7 36.7
P 4B - P 4X		.175 .285 .296	.184 .323 .333	-.290 - .100 - .196	- .620 - .439 - .446	.167 - .205 .310	.136 .248 .250	- .239 - .885E-01 - .138
EC1B - EC1X		-.310E-01 - .828E-01 .230	- .260E-01 - .198E-01 - .321E-01	.339E-01 .741E-01 .218E-01	.131E-01 .245E-01 .262E-01	.630E-02 .181E-01 - .209E-01	.116E-01 .677E-02 .919E-02	.407E-01 - .344E-01 - .959E-01

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Case C

CALCULATION-TO-EXPERIMENT DATA UNCERTAINTY ANALYSIS FOR NRC/ICAP

FIRST LINE : DIFFERENCE BETWEEN CALCULATED AND (AVERAGED) EXPERIMENTAL DATA AT END OF THE INTERVAL
 SECOND LINE : MEAN DIFFERENCE OVER THE INTERVAL
 THIRD LINE : MEAN SIGMA OVER THE INTERVAL (ROOT MEAN SQUARE OF THE DIFFERENCE)

- CODES -		- - - - TIME INTERVAL - - - -					
GALC.	EXP.	0.0 - 20.00	- 80.00	- 200.0	- 500.0	- 1000.	- 1800
C 30 - C 3X		-3.53 -4.19 4.43	-3.81 -4.21 4.26	-980 -829 .958	-6.12 -3.43 3.85	-4.88 -6.84 6.71	-1.28 -2.70 2.90
C 40 - C 4X		8.07 12.9 14.7	1.91 4.29 4.82	.440 1.17 1.92	-6.02 -2.13 2.76	-3.87 -5.45 6.52	-800E-01 -1.42 1.84
C 50 - C 5X		2.88 8.84 10.3	1.29 3.01 3.18	.250 825 -982	-5.24 -2.35 2.93	-4.06 -9.66 6.72	-1.30 -1.54 1.94
C 60 - C 6X		3.63 10.4 12.0	1.27 3.06 3.37	.480 1.17 1.29	-4.87 -2.04 2.69	-3.88 -5.23 6.30	-180 -1.23 1.68
C 90 - C 9X		-4.20 -1.74 3.49	-2.17 -2.52 2.78	-2.76 -2.17 2.21	-7.61 -6.07 6.34	-6.04 -8.00 8.05	-2.23 -3.77 3.96
C AC - C AX		-3.03 1.09 1.88	.926 .467 2.69	-.991 -914E-01 -838	1.08 .256 .771	1.84 3.02 3.09	2.28 3.31 3.33
V 30 - V 3X		-5.80 -1.55 -1.88	4.98 1.79 2.16	15.9 10.3 12.7	14.3 12.2 12.6	-7.56 4.98 10.6	-1.25 -4.00 4.26
V 60 - V 6X		-4.37 -1.29 2.23	-1.84 -2.59 3.47	-2.74 -2.02 2.08	-7.54 -6.09 6.36	-6.07 -8.03 8.08	-2.28 -3.82 4.01
V 70 - V 7X		7.87 6.40 6.49	3.87 5.60 6.06	3.04 3.24 3.25	2.86 2.76 2.76	1.77 2.17 2.19	642 1.17 1.22
V 80 - V 8X		-3.35 -2.28 2.43	-2.87 -5.08 3.11	-1.75 -1.93 2.00	-8.92 -6.45 8.83	-8.01 -10.1 10.1	-4.66 -6.13 6.22
V 90 - V 9X		.365 .602 .619	.114 .314 .353	-740E-02 -716E-01 -924E-01	-.611 -.259 -.309	-.260 -.613 -.621	-.974E-01 -.172 -.189
V AC - V AX		.412 .628 .645	-.188 -.377 -.408	-.784E-01 .163 .162	-.478 -.178 -.249	-.266 -.446 -.455	-.142E-01 -864E-01 123
HL10 - HL1X		69.5 72.5 73.3	107. 109. 106.	63.6 70.8 71.9	313. 116. 120.	651. 627. 649.	692. 684. 684.
HL20 - HL2X		39.3 43.1 43.5	37.3 37.0 37.1	120. 85.3 92.4	207. 104. 109.	405. 437. 435.	409. 430. 430.
HL30 - HL3X		14.6 11.7 12.2	-14.0 -13.2 17.1	-21.1 -18.9 16.0	-42.0 -38.3 38.7	-46.7 -44.3 44.3	-84.1 -30.7 40.8
HL40 - HL4X		-3.20 2.29 2.78	1.21 1.29 1.92	.910 1.65 1.63	-4.56 -1.77 2.64	-9.86 -6.27 6.58	-16.9 -13.6 13.9
HL60 - HL6X		.322 .862 .883	-.699E-01 -.266 -.310	-.421E-01 -.342E-01 -.637E-01	-.638 -.291 -.337	-.356 -.638 -.646	-.106 -.161 -.200
CL10 - CL1X		84.6 71.3 71.4	83.4 87.2 87.9	-172. 37.0 162.	-266. -274. 277.	-126. -181. 189.	-74.1 -98.6 101.
CL30 - CL3X		30.3 33.1 33.8	89.4 42.1 43.8	-431. -382. 404.	384. -405. 406.	-181. -261. 269.	-155. -167. 163.
CL40 - CL4X		-.877E-01 .233 .266	.327E-01 -.313E-01 .370E-01	-.362E-02 -.105E-01 -.141E-01	-.278E-01 -.123E-01 -.148E-01	-.526E-01 -.257E-01 -.275E-01	-.666E-01 -.615E-01 -.633E-01
CL60 - CL6X		-1.58 -1.90 1.81	-1.10 -1.18 1.19	-1.02 -1.04 1.04	-.477 -.780 -.775	-.171 -.299 -.317	-.170E-02 -.862E-01 -.102
CL80 - CL8X		1.20 .930 .857	1.50 1.55 1.56	1.86 1.86 1.85	-6.21 -6.40 6.66	-8.61 -11.0 11.6	-2.07 -6.47 10.3
CL70 - CL7X		.469 .590 .705	.214 .419 .448	-.122 -.187 -.195	-.389 -.139 -.9	-.206 -.388 .399	-.434E-01 -.367E-01 .895E-01
CL80 - CL8X		.662 .793 .607	.320 .508 .532	.211 .280 .285	-.291 -432E-01 .172	-.103 -.284 -.300	-.163 -766E-01 -.114
CL90 - CL9X		2.22 10.4 14.6	-9.70 -8.33 8.94	-10.1 -9.95 9.95	-9.56 -9.67 9.67	-10.4 -10.1 10.1	-11.1 -10.7 10.7
CLAC - CLAX		.227 166. 160.	-8.94 15.1 75.4	63.7 40.6 55.4	-.655E-03 9.91 9.3	.124 -.184 -.684	.267 -1.54 2.21

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- CODES -		- - - - TIME INTERVAL - - - -					
CALC.	EXP.	0.0 - 20.00	- 80.00	- 200.0	- 510.0	- 1000.	- 1500.
BR1C - BR1X		-4.07 33.9 45.8	-25.7 -18.9 17.2	88.0 23.6 94.4	-68.3 -79.1 99.8	-36.6 -3.00 39.6	22.4 17.4 28.9
BR2C - BR2X		7.07 5.46 6.70	1.40 2.98 3.31	-1.72 273 1.62	-1.65 -1.91 1.94	-3.17 -1.995 1.12	-1.604 -1.498 1.637
BR4C - BR4X		860 -11.3 17.7	1.37 1.20 1.23	830 842 874	-4.65 -1.78 2.83	-3.88 -4.90 6.23	-5.65 -1.98 6.40
BR5C - BR5X		2.99 16.7 22.1	1.12 2.72 2.90	774 1.32 1.38	1.19 1.04 1.06	1.19 1.28 2.04	2.22 2.25 6.89
BR6C - BR6X		.823 .832 .861	.267 .452 .476	.175 .225 .233	-3.309 -6.56E-01 .178	-1.180 -1.297 .312	.114 -2.41E-01 1.803E-01
SP1C - SP1X		-7.34 -8.28 6.39	-1.10 -2.13 2.72	-4.70 -7.09 8.02	-6.73 -3.20 3.63	-10.7 -8.10 8.19	-10.9 -15.4 16.6
SP2C - SP2X		-7.09 -2.98 3.61	-1.85 -2.02 2.60	2.08 1.90 1.32	2.66 3.28 2.30	3.35 3.64 3.73	-1.373 1.312 1.19
SP3C - SP3X		-2.77 7.81 13.2	-11.9 -10.4 10.7	-12.5 -13.1 13.1	-8.92 -10.8 10.8	-9.19 -10.4 10.4	-7.73 -8.65 8.71
SS3C - SS3X		-418 -364 422	-368 -387 381	-340 -326 330	-278 -315 315	-285 -291 292	-241 -249 249
SS4C - SS4X		13.3 6.83 9.33	-670 8.43 6.85	-7.12 -4.16 4.64	-6.24 -6.91 6.93	-3.27 -5.49 6.67	1.26 -1.684 1.70
SS5C - SS5X		.267 -5.48E-02 1.02	.223 .270 .271	.142 .208 .212	-350 -1.05 1.95	-744 -538 647	-1.26 -983 1.00
S 1C - S 1X		-20.6 -14.1 14.8	-437 -7.66 9.45	8.66 3.44 4.19	175 2.71 4.33	-7.60 -2.60 3.48	-20.2 -14.4 14.9
P 1C - P 1X		.820E-01 .617E-01 .658E-01	.120E-02 .206E-01 .589E-01	-556E-03 .104E-03 .635E-03	-299E-03 -269E-03 .330E-03	-476E-03 .692E-04 227E-03	493E-03 197E-03 265E-03
P 2C - P 2X		-19.7 -11.9 12.6	-1.88 -11.8 14.4	-8.96 -4.87 6.26	-37.6 -23.2 21.2	-61.3 -51.4 51.6	-76.9 -68.7 68.9
P 3C - P 3X		-19.3 -12.8 13.4	-1.22 -11.6 14.1	1.47 1.74 1.02	-11.4 -4.29 6.02	-21.8 -17.5 17.7	-20.7 -25.3 25.4
P 4C - P 4X		249 302 311	126 330 361	293E-01 103 116	-481 -224 279	-318 -478 487	-443E-01 -130 154
EC1C - EC1X		.310E-01 -564E-01 .198	-226E-01 -178E-01 297E-01	162E-01 237E-02 987E-02	112E-01 119E-01 154E-01	349E-01 347E-01 355E-01	215E-01 287E-01 289E-01

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Description of the Accompanying Data Package

STUDSVIK

THIS TAPE CONTAINS DATA FROM THE ICAP PREDICTION CALCULATION
WITH THE RELAP5/MOD2/36.04 FOR THE LOFT EXPERIMENT NO. L3-5.

CONTENTS, FILE	1.	THIS DESCRIPTIVE TEXT
	2.	INPUT CASE A, STEADY STATE
	3.	- " - B, - " -
	4.	- " - C, - " -
	5.	DATA, EXPERIMENT
	6.	- " - , CASE A
	7.	- " - , CASE B
	8.	- " - , CASE C

I. COMPUTER		
NAME		CYBER 170-810
WORD SIZE		60

II. TAPE FORMAT		
NUMBER OF TRACKS		9
PACKING DENSITY		1600 BPI
RECORD SIZE		80
BLOCKING FACTOR		64
CODED		EBCDIC
CONTROL WORDS		NO

III. DATA FORMAT, FOR EACH OF THE FILES 5 THROUGH 8

TITLE RECORD(S), (FORMAT IS,A75)
FIELD 1, THE NUMBER OF DATA CHANNELS ON THE FILE
FIELD 2, PROBLEM IDENTIFICATION
UP TO FIVE ADDITIONAL IDENTIFICATION RECORDS
MAY BE ADDED BY 'C' IN COLUMN 1 OF FIELD 1

DATA SET RECORD 1, (FORMAT 215,A60)
FIELD 1, NUMBER OF DATA POINTS
FIELD 2, THE ENGINEERING UNIT CODE (EUC) FOR THE
VARIABLE
FIELD 3, IDENTIFYING TEXT OF THE DATA
REMAINING DATA SET RECORDS FORMAT 5(E16.9)

EACH DATA CHANNEL SUBMITTED IS GIVEN THROUGH TWO DATA
SETS, THE FIRST OF WHICH IS THE TIME DATA SET.
THE TWO SETS HAVE THE SAME NUMBER OF DATA POINTS.
THE TIME DATA SET IS IDENTIFIED BY EUC=77 (FIELD 2)
AND THE IDENTIFYING TEXT 'TIME' (FIELD 3).

BIBLIOGRAPHIC DATA SHEET

(See instructions on the reverse)

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(Assigned by NRC. Add Vol., Supp., Rev.,
and Addendum Numbers, if any.)

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Small Break Experiment L3-5

3. DATE REPORT PUBLISHED

MONTH	YEAR
March	1992

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10. SUPPLEMENTARY NOTES

11. ABSTRACT (200 words or less)

An independent assessment of the RELAP5/MOD2 code was conducted by Studsvik Energiteknik AB. The LOFT small break experiment L3-5 was assessed using the RELAP5/MOD2 code. Three calculations were carried out; one base case calculation and two sensitivity calculations with model changes. The transient predictions compare reasonably well with the experiment as regards firsthand parameters such as system pressures and fluid temperatures. Variations are enumerated and discussed.

12. KEY WORDS/DESCRIPTORS (List words or phrases that will assist researchers in locating the report.)

ICAP Program
RELAP5/MOD2 Computer Code
Small Break Experiment

13. AVAILABILITY STATEMENT

Unlimited

14. SECURITY CLASSIFICATION

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Unclassified

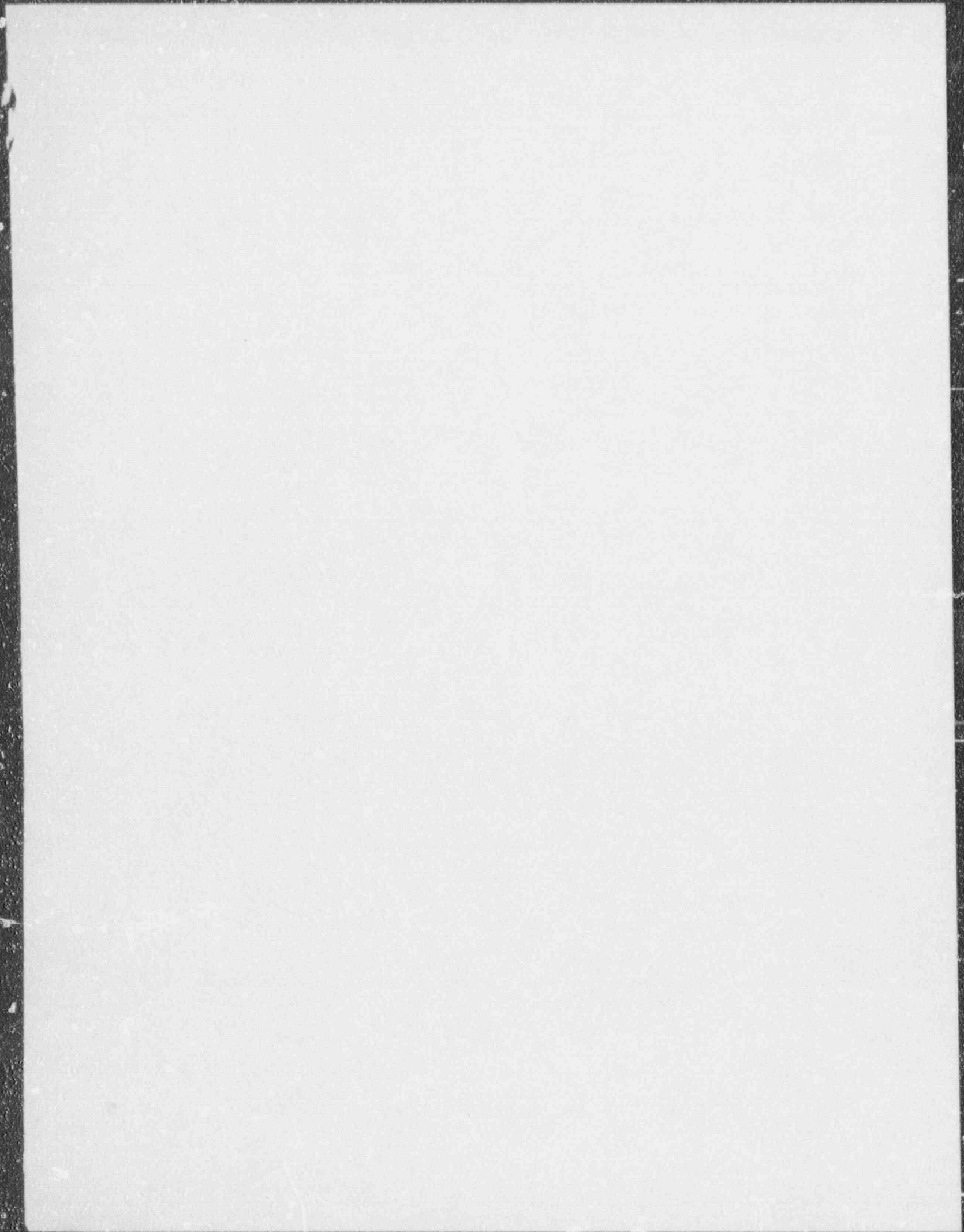
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