

JUL 03 1984

7/16

50-298

Nebraska Public Power District
ATTN: J. M. Pilant, Manager, Technical
Staff-Nuclear Power Group
P.O. Box 499
Columbus, Nebraska 68601

Gentlemen:

SUBJECT: Cooper-Operator Licensing Examination Report Addendum

The May 11, 1984, Operator Licensing Examination Report inadvertently omitted the figures, charts, and tables that were provided to candidates as part of the reactor and senior reactor operator examinations administered in March of this year. Enclosed is one copy of this material which should be added to the examination master copy provided in our May 11 letter. We regret any inconvenience this may have caused you.

In accordance with 10 CFR 2.790(a), a copy of this letter and the enclosure will be placed in the NRC Public Document Room unless you notify this office by telephone within 10 days of the date of this letter and submit written application to withhold information contained herein within 30 days of the date of this letter. Such application must be consistent with the requirements of 10 CFR 2.790(b)(1).

Should you have any questions concerning this letter, please contact us.

Sincerely,

Original Signed By
E. H. Johnson
E. H. Johnson, Chief
Reactor Project Branch 1

Enclosure:
Examination master copy figures, charts, and tables

cc:
Paul V. Thomason, Division Manager
of Nuclear Operations
Cooper Nuclear Station
P.O. Box 98
Brownville, Nebraska 68321

R. Beilke, Training Manager (Same address)

bcc: DMB M003
R. Cooley RPB1 RPB2
J. Pellet Section Chief RIV File
E. Haycraft R. Denise J. Collins
R. Eaton, OLB TPB RRI
Kansas State Dept. of Health
Nebraska State Dept. of Health

RPB2 *JP* RPB2 *RAC* RPB2 *EJ* RPB1 *EJ*
JPellet/vs RCooley EHJohnson EHJohnson
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M003
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SIMPLIFIED SCHEMATIC OF MODIFIED
CRD HYDRAULIC SYSTEM

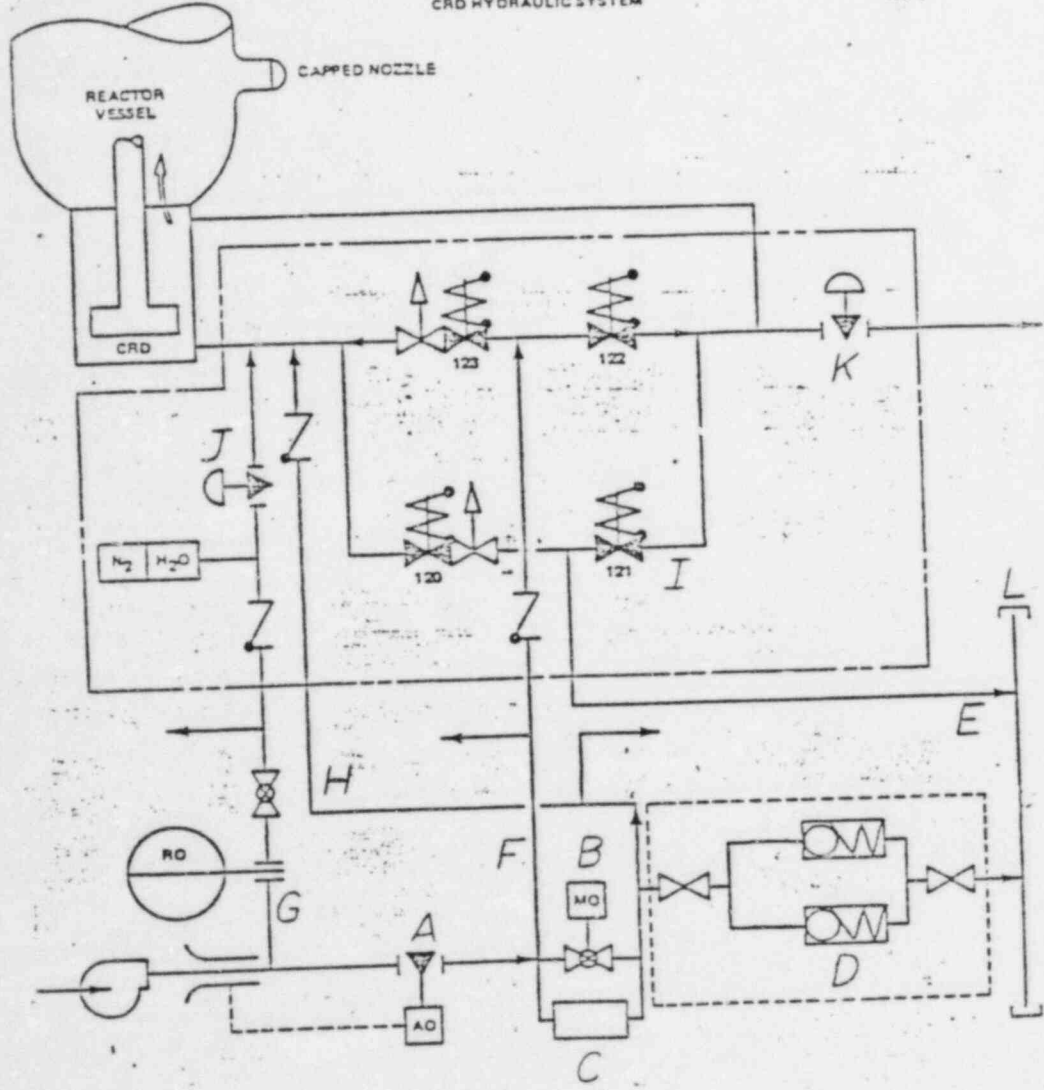


Figure 1B

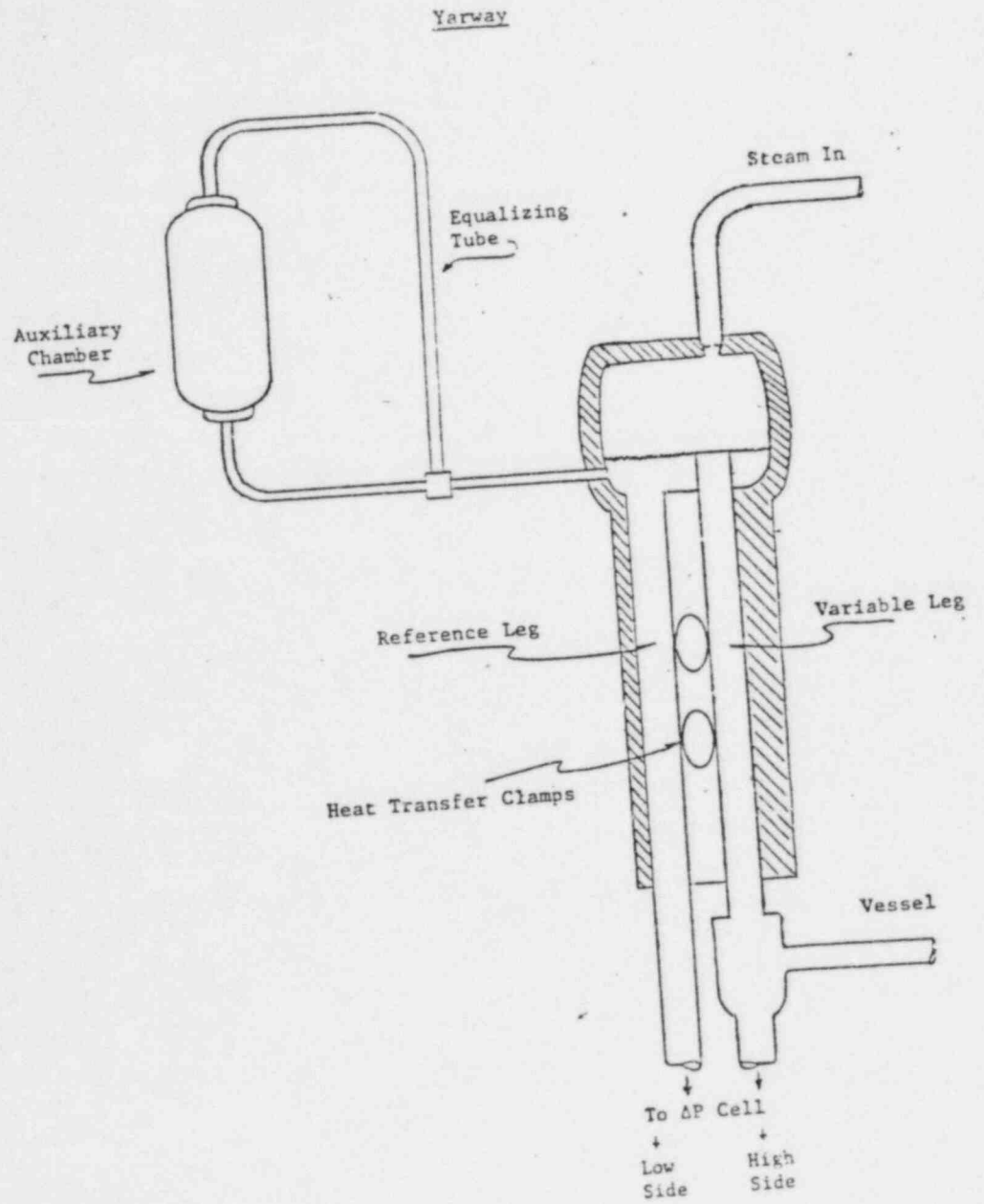


FIGURE 6

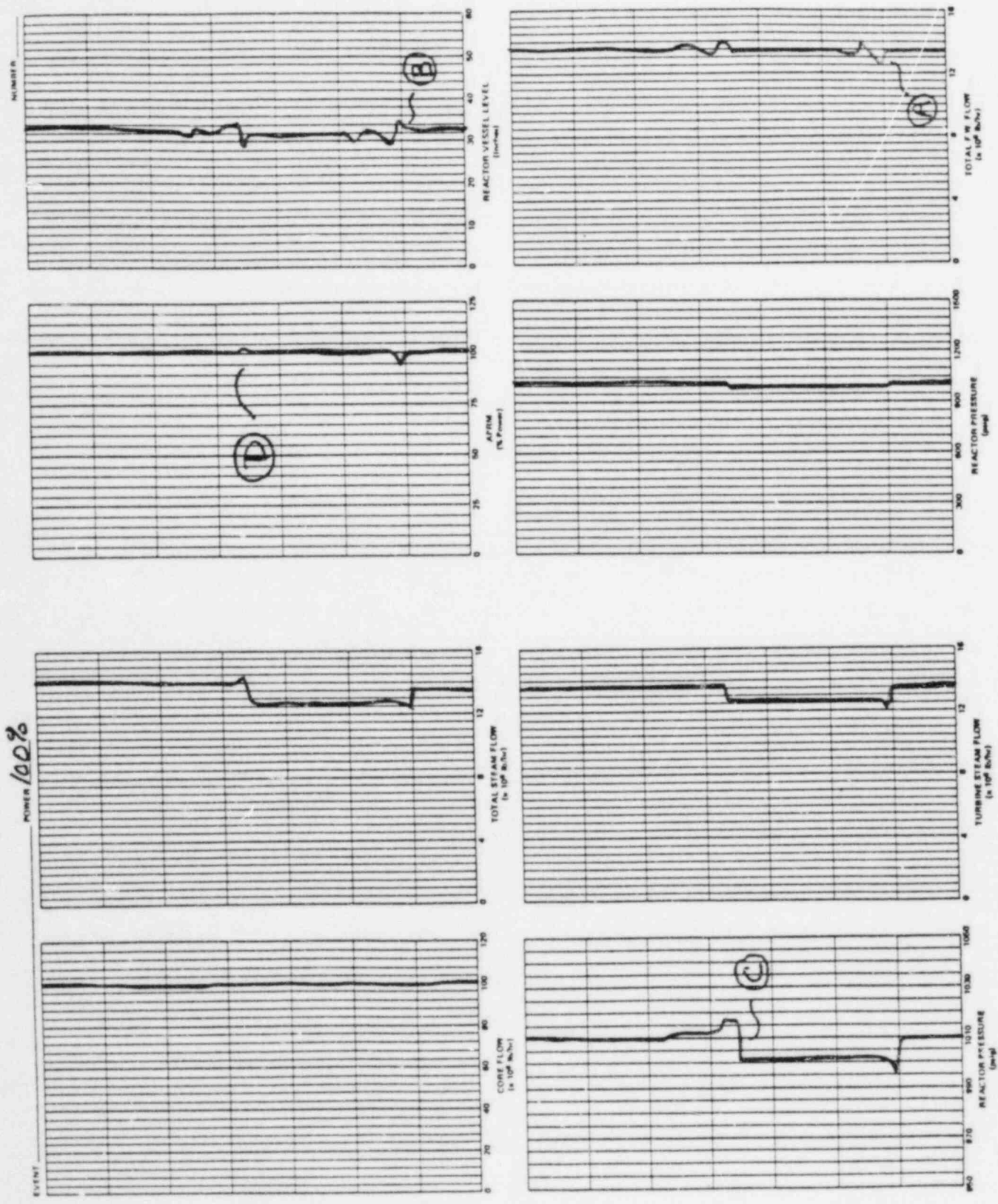


FIGURE 7

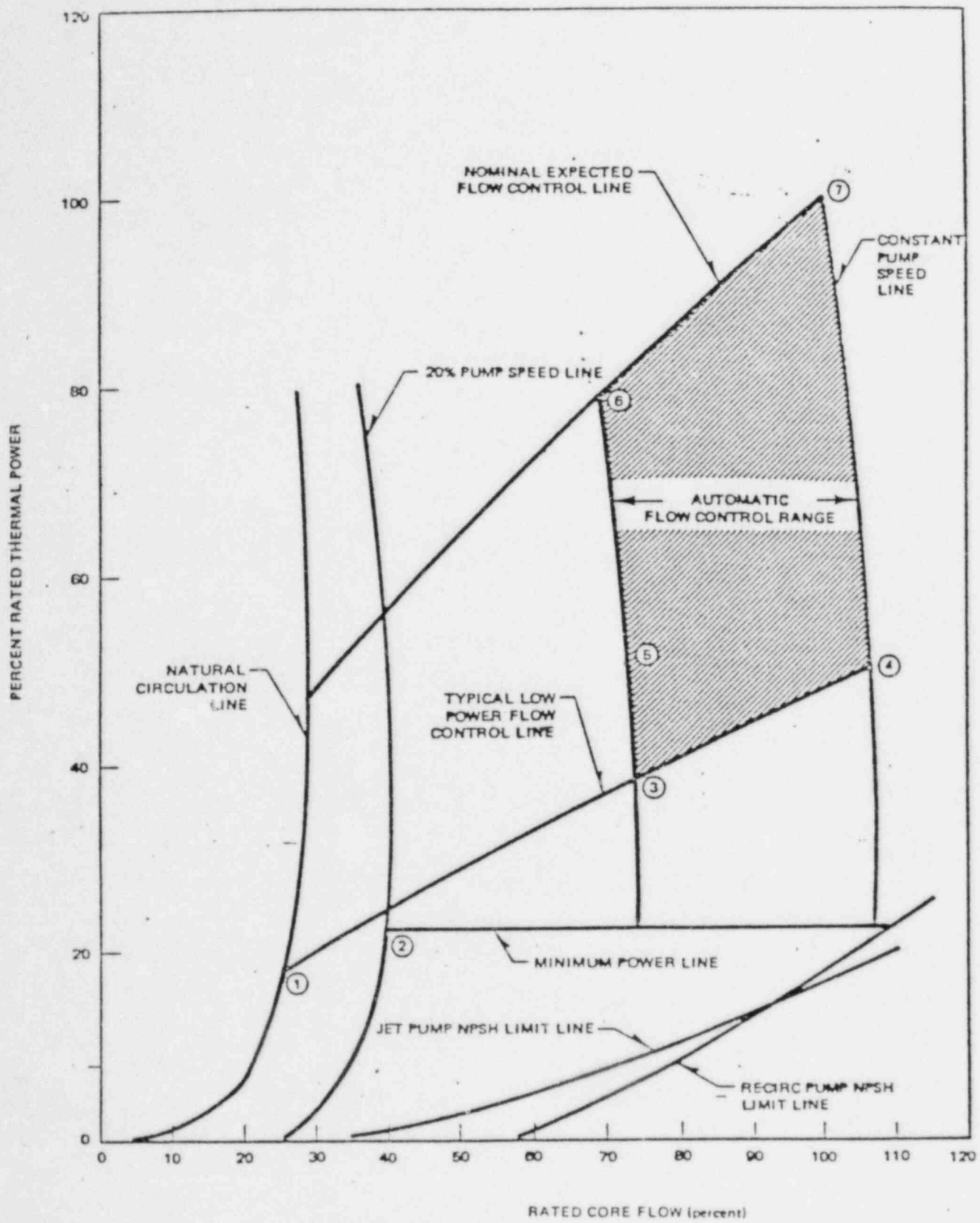


Figure 11 NORMAL OPERATING MAP

Properties of Saturated Steam and Saturated Water

Pressure Lbs. per Sq. In.	Temperature t	Heat of the Liquid Evaporation	Total Heat h _g	Specific Volume Δ	Gage	
					p	p'
Absolute		Degrees F		Cu. ft. per lb.		
p	t	Btu/lb	Btu/lb	Water	Steam	
150.0	353.3	825.0	1201.3	0.01865	1.84317	
155.0	358.0	820.0	1201.7	0.01868	1.80802	
160.0	362.7	815.0	1202.1	0.01875	1.77418	
165.0	367.4	810.0	1202.5	0.01882	1.74157	
170.0	372.1	805.0	1202.9	0.01888	1.71013	
175.0	376.8	800.0	1203.3	0.01895	1.67978	
180.0	381.5	795.0	1203.7	0.01901	1.65049	
185.0	386.2	790.0	1204.1	0.01907	1.62218	
190.0	390.9	785.0	1204.5	0.01913	1.59482	
195.0	395.6	780.0	1204.9	0.01919	1.56835	
200.0	400.3	775.0	1205.3	0.01925	1.54274	
205.0	405.0	770.0	1205.7	0.01931	1.51795	
210.0	409.7	765.0	1206.1	0.01937	1.49398	
215.0	414.4	760.0	1206.5	0.01943	1.47074	
220.0	419.1	755.0	1206.9	0.01949	1.44821	
225.0	423.8	750.0	1207.3	0.01955	1.42637	
230.0	428.5	745.0	1207.7	0.01961	1.40513	
235.0	433.2	740.0	1208.1	0.01967	1.38449	
240.0	437.9	735.0	1208.5	0.01973	1.36445	
245.0	442.6	730.0	1208.9	0.01979	1.34491	
250.0	447.3	725.0	1209.3	0.01985	1.32587	
255.0	452.0	720.0	1209.7	0.01991	1.30733	
260.0	456.7	715.0	1210.1	0.01997	1.28929	
265.0	461.4	710.0	1210.5	0.02003	1.27175	
270.0	466.1	705.0	1210.9	0.02009	1.25471	
275.0	470.8	700.0	1211.3	0.02015	1.23817	
280.0	475.5	695.0	1211.7	0.02021	1.22213	
285.0	480.2	690.0	1212.1	0.02027	1.20659	
290.0	484.9	685.0	1212.5	0.02033	1.19155	
295.0	489.6	680.0	1212.9	0.02039	1.17691	
300.0	494.3	675.0	1213.3	0.02045	1.16267	
305.0	499.0	670.0	1213.7	0.02051	1.14883	
310.0	503.7	665.0	1214.1	0.02057	1.13539	
315.0	508.4	660.0	1214.5	0.02063	1.12235	
320.0	513.1	655.0	1214.9	0.02069	1.10971	
325.0	517.8	650.0	1215.3	0.02075	1.09747	
330.0	522.5	645.0	1215.7	0.02081	1.08563	
335.0	527.2	640.0	1216.1	0.02087	1.07419	
340.0	531.9	635.0	1216.5	0.02093	1.06315	
345.0	536.6	630.0	1216.9	0.02099	1.05241	
350.0	541.3	625.0	1217.3	0.02105	1.04207	
355.0	546.0	620.0	1217.7	0.02111	1.03213	
360.0	550.7	615.0	1218.1	0.02117	1.02259	
365.0	555.4	610.0	1218.5	0.02123	1.01345	
370.0	560.1	605.0	1218.9	0.02129	1.00471	
375.0	564.8	600.0	1219.3	0.02135	0.99637	
380.0	569.5	595.0	1219.7	0.02141	0.98843	
385.0	574.2	590.0	1220.1	0.02147	0.98089	
390.0	578.9	585.0	1220.5	0.02153	0.97375	
395.0	583.6	580.0	1220.9	0.02159	0.96691	
400.0	588.3	575.0	1221.3	0.02165	0.96037	
405.0	593.0	570.0	1221.7	0.02171	0.95413	
410.0	597.7	565.0	1222.1	0.02177	0.94819	
415.0	602.4	560.0	1222.5	0.02183	0.94255	
420.0	607.1	555.0	1222.9	0.02189	0.93721	
425.0	611.8	550.0	1223.3	0.02195	0.93217	
430.0	616.5	545.0	1223.7	0.02201	0.92743	
435.0	621.2	540.0	1224.1	0.02207	0.92299	
440.0	625.9	535.0	1224.5	0.02213	0.91885	
445.0	630.6	530.0	1224.9	0.02219	0.91491	
450.0	635.3	525.0	1225.3	0.02225	0.91117	
455.0	640.0	520.0	1225.7	0.02231	0.90763	
460.0	644.7	515.0	1226.1	0.02237	0.90429	
465.0	649.4	510.0	1226.5	0.02243	0.90115	
470.0	654.1	505.0	1226.9	0.02249	0.89821	
475.0	658.8	500.0	1227.3	0.02255	0.89547	
480.0	663.5	495.0	1227.7	0.02261	0.89293	
485.0	668.2	490.0	1228.1	0.02267	0.89059	
490.0	672.9	485.0	1228.5	0.02273	0.88845	
495.0	677.6	480.0	1228.9	0.02279	0.88651	
500.0	682.3	475.0	1229.3	0.02285	0.88477	
505.0	687.0	470.0	1229.7	0.02291	0.88323	
510.0	691.7	465.0	1230.1	0.02297	0.88189	
515.0	696.4	460.0	1230.5	0.02303	0.88075	
520.0	701.1	455.0	1230.9	0.02309	0.87981	
525.0	705.8	450.0	1231.3	0.02315	0.87907	
530.0	710.5	445.0	1231.7	0.02321	0.87853	
535.0	715.2	440.0	1232.1	0.02327	0.87819	
540.0	720.0	435.0	1232.5	0.02333	0.87805	
545.0	724.7	430.0	1232.9	0.02339	0.87801	
550.0	729.4	425.0	1233.3	0.02345	0.87807	
555.0	734.1	420.0	1233.7	0.02351	0.87823	
560.0	738.8	415.0	1234.1	0.02357	0.87849	
565.0	743.5	410.0	1234.5	0.02363	0.87885	
570.0	748.2	405.0	1234.9	0.02369	0.87931	
575.0	752.9	400.0	1235.3	0.02375	0.87987	
580.0	757.6	395.0	1235.7	0.02381	0.88053	
585.0	762.3	390.0	1236.1	0.02387	0.88129	
590.0	767.0	385.0	1236.5	0.02393	0.88215	
595.0	771.7	380.0	1236.9	0.02399	0.88311	
600.0	776.4	375.0	1237.3	0.02405	0.88417	
605.0	781.1	370.0	1237.7	0.02411	0.88533	
610.0	785.8	365.0	1238.1	0.02417	0.88659	
615.0	790.5	360.0	1238.5	0.02423	0.88795	
620.0	795.2	355.0	1238.9	0.02429	0.88941	
625.0	800.0	350.0	1239.3	0.02435	0.89097	
630.0	804.7	345.0	1239.7	0.02441	0.89263	
635.0	809.4	340.0	1240.1	0.02447	0.89439	
640.0	814.1	335.0	1240.5	0.02453	0.89625	
645.0	818.8	330.0	1240.9	0.02459	0.89821	
650.0	823.5	325.0	1241.3	0.02465	0.90027	
655.0	828.2	320.0	1241.7	0.02471	0.90243	
660.0	833.0	315.0	1242.1	0.02477	0.90469	
665.0	837.7	310.0	1242.5	0.02483	0.90705	
670.0	842.4	305.0	1242.9	0.02489	0.90951	
675.0	847.1	300.0	1243.3	0.02495	0.91207	
680.0	851.8	295.0	1243.7	0.02501	0.91473	
685.0	856.5	290.0	1244.1	0.02507	0.91749	
690.0	861.2	285.0	1244.5	0.02513	0.92035	
695.0	865.9	280.0	1244.9	0.02519	0.92331	
700.0	870.6	275.0	1245.3	0.02525	0.92637	
705.0	875.3	270.0	1245.7	0.02531	0.92953	
710.0	880.0	265.0	1246.1	0.02537	0.93279	
715.0	884.7	260.0	1246.5	0.02543	0.93615	
720.0	889.4	255.0	1246.9	0.02549	0.93961	
725.0	894.1	250.0	1247.3	0.02555	0.94317	
730.0	898.8	245.0	1247.7	0.02561	0.94683	
735.0	903.5	240.0	1248.1	0.02567	0.95059	
740.0	908.2	235.0	1248.5	0.02573	0.95445	
745.0	912.9	230.0	1248.9	0.02579	0.95841	
750.0	917.6	225.0	1249.3	0.02585	0.96247	
755.0	922.3	220.0	1249.7	0.02591	0.96663	
760.0	927.0	215.0	1250.1	0.02597	0.97089	
765.0	931.7	210.0	1250.5	0.02603	0.97525	
770.0	936.4	205.0	1250.9	0.02609	0.97971	
775.0	941.1	200.0	1251.3	0.02615	0.98427	
780.0	945.8	195.0	1251.7	0.02621	0.98893	
785.0	950.5	190.0	1252.1	0.02627	0.99369	
790.0	955.2	185.0	1252.5	0.02633	0.99855	
795.0	960.0	180.0	1252.9	0.02639	1.00351	
800.0	964.7	175.0	1253.3	0.02645	1.00857	
805.0	969.4	170.0	1253.7	0.02651	1.01373	
810.0	974.1	165.0	1254.1	0.02657	1.01909	
815.0	978.8	160.0	1254.5	0.02663	1.02455	
820.0	983.5	155.0	1254.9	0.02669	1.03011	
825.0	988.2	150.0	1255.3	0.02675	1.03577	
830.0	993.0	145.0	1255.7	0.02681	1.04153	
835.0	997.7	140.0	1256.1	0.02687	1.04739	
840.0	1002.4	135.0	1256.5	0.02693	1.05335	
845.0	1007.1	130.0	1256.9	0.02699	1.05941	
850.0	1011.8	125.0	1257.3	0.02705	1.06557	
855.0	1016.5	120.0	1257.7	0.02711	1.07183	
860.0	1021.2	115.0	1258.1	0.02717	1.07819	
865.0	1025.9	110.0	1258.5	0.02723	1.08465	
870.0	1030.6	105.0	1258.9	0.02729	1.09121	
875.0	1035.3	100.0	1259.3	0.02735	1.09787	
880.0	1040.0	95.0	1259.7	0.02741	1.10463	
885.0	1044.7	90.0	1260.1	0.02747	1.11149	
890.0	1049.4	85.0	1260.5	0.02753	1.11845	
895.0	1054.1	80.0	1260.9	0.02759	1.12551	
900.0	1058.8	75.0	1261.3	0.02765	1.13267	
905.0	1063.5	70.0	1261.7	0.02771	1.13993	
910.0	1068.2	65.0	1262.1	0.02777	1.14729	
915.0	1072.9	60.0	1262.5	0.02783	1.15475	
920.0	1077.6	55.0	1262.9	0.02789	1.16231	
925.0	1082.3	50.0	1263.3	0.02795	1.17007	
930.0	1087.0	45.0	1263.7	0.02801	1.17793	
935.0	1091.7	40.0	1264.1	0.02807	1.18589	
940.0	1096.4	35.0	1264.5	0.02813	1.19395	
945.0	1101.1	30.0	1264.9	0.02819	1.20211	
950.0	1105.8	25.0	1265.3	0.02825	1.21037	
955.0	1110.5	20.0	1265.7	0.02831	1.21873	
960.0	1115.2	15.0	1266.1	0.02837	1.22719	
965.0	1119.9	10.0	1266.5	0.02843	1.23575	
970.0	1124.6	5.0	1266.9	0.02849	1.24441	
975.0	1129.3	0.0	1267.3	0.02855	1.25317	
980.0	1134.0		1267.7	0.02861	1.26203	
985.0	1138.7		1268.1	0.02867	1.27099	
990.0	1143.4		1268.5	0.02873	1.28005	
995.0	1148.1		1268.9	0.02879	1.28921	
1000.0	1152.8		1269.3	0.02885	1.29847	
1005.0	1157.5		1269.7	0.02891	1.30783	
1010.0	1162.2		1270.1	0.02897	1.	

Material	Half-Life	Energy MEV per disintegration	Table I		Table II	
			Col I Air μc/ml	Col II Water μc/ml	Col I Air μc/ml	Col II Water μc/ml
A-41	1.83 h	1.3	2×10^{-6}		4×10^{-8}	
Co-60	5.3 y	2.5	3×10^{-7}	1×10^{-3}	1×10^{-8}	5×10^{-5}
I-131	8.1 d	0.36	9×10^{-9}	6×10^{-5}	1×10^{-10}	3×10^{-7}
Kr-85	10.8 y	0.04	1×10^{-5}		3×10^{-7}	
Ni-65	2.5 h	0.59	9×10^{-7}	4×10^{-3}	3×10^{-8}	1×10^{-4}
Pu-239	2.4×10^4 y	0.008	2×10^{-12}	1×10^{-4}	6×10^{-14}	5×10^{-6}
Sr-90	28 y		1×10^{-9}	1×10^{-5}	3×10^{-11}	3×10^{-6}
Xe-135	9.2 h	0.25	4×10^{-6}		1×10^{-7}	
Any single radionuclide with $T_{1/2} > 2$ hr which does not decay by α or spontaneous fission			3×10^{-9}	5×10^{-5}	1×10^{-10}	3×10^{-6}

Neutron Energy (MEV)	Neutrons per cm ² equivalent to 1 rem	Average flux to deliver 100 rem in 40 hours
Thermal	970×10^6	670
0.02	400×10^6	280
0.5	43×10^6	30
10	24×10^6	17

LINEAR ABSORPTION COEFFICIENTS (cm⁻¹)

Energy (MEV)	Water	Concrete	Iron	Lead
0.5	0.090	0.21	0.63	1.7
1.0	0.067	0.15	0.44	0.77
1.5	0.057	0.13	0.40	0.57
2.0	0.048	0.11	0.33	0.51
2.5	0.042	0.097	0.31	0.47
3.0	0.038	0.088	0.30	0.47

FORMULAS AND CONVERSIONS

$$r/hr = \frac{6CE}{d^2} \quad I_x = I_0 e^{-\mu x} \quad I_x = \frac{I_0}{d^2} \quad N = N_0 e^{-\lambda t}$$

$$T_{1/2} = \frac{0.693}{\lambda} \quad p = \frac{\sum \phi V}{3 \times 10^{10}} \quad T = \frac{\theta - e}{\lambda e}$$

$$T = \frac{l^*}{e} + \frac{\theta - e}{\lambda e} \quad e = \frac{1}{Tk} + \sum \frac{\theta_i}{1 + \lambda T} \quad T = \frac{l}{e - \theta}$$

1 gal = 3.78 liters
 1 in = 2.54 cm
 1 yr = 3.15×10^7 sec.

1 kg = 2.21 lbs
 1 μm/cm³ = 62.4 lbs/ft³
 1 ft³ = 7.48 gal

$N_A = 6.03 \times 10^{23}$
 $\pi = 3.14$
 $e = 2.72$

$$t^* = 10^{-3} \text{ seconds}$$

$$A = A_0 e^{-\lambda t}$$

$$E = mc^2$$

$$A = \lambda N$$

$$\Delta E = 931 \Delta M$$

$$I = I_0 e^{-\mu x}$$

$$I = I_0 e^{-\Gamma x}$$

$$OH^- \quad H^+ = 10^{-14}$$

$$S.C.R. = \frac{S}{1 - K_{eff}}$$

$$t_{eff} = \frac{(t_h)(t_b)}{t_h + t_b}$$

$$E = IR$$

$$P = IE$$

$$P = \frac{E^2}{R}$$

$$\bar{\tau} \approx 12.7 \text{ sec.}$$

$$\Sigma = \sigma N$$

$$V = \frac{e}{c}$$

$$ER = I\phi$$

$$V_F = V_0 + at$$

$$S = V_0 T + \frac{1}{2} at^2$$

$$a = \frac{V_F - V_0}{t}$$

$$W = Mg$$

$$F = Ma$$

$$P = P_0 e^{c/\tau}$$

$$W = \frac{\theta}{t}$$

$$W = P_s$$

$$P = \frac{W}{t}$$

$$\bar{\lambda} = 0.1 \text{ seconds}^{-1}$$

$$R_t = \frac{R_1 R_2}{R_1 + R_2}$$

$$C_1(1-K_1) = C_2(1-K_2)$$

$$P = P_0 10^{\text{SUR}(t)}$$

$$M = \frac{1}{1-K} = \frac{C}{C_0}$$

$$I = I_0 10^{-\frac{x}{TVL}}$$

$$Q = U \Delta t$$

$$\lambda = \frac{0.693}{t_{1/2}}$$

$$P = \frac{2\phi v}{3 \times 10^{10}}$$

$$\frac{C_0}{C_1} = \frac{1-K_1}{1-K_0}$$

$$KE = \frac{1}{2} mv^2$$

$$I_t = I_1 + I_2 + \dots + I_n$$

$$\Delta p = \frac{K_2 - K_1}{K_2 - K_1}$$

$$\lambda = \frac{0.693}{1-p}$$

$$TVL = \frac{2.3}{\mu}$$

MISCELLANEOUS CONVERSIONS

Density H₂O = 62.4 lb/ft³

Heat of Vaporization H₂O = 970 BTU/lb.

Heat of Fusion H₂O = 144 BTU/lb.

Watts = BTU/hr x .293

H. P. = BTU/hr x 3.93 x 10⁻⁶

KW = H. P. x .7457

MW = 3.41 x 10⁶ BTU/hr

TVT lead=1.5"

PWR. = $\dot{m} \Delta h$

PWR. = $W_F \Delta h$

BTU/lb = Cal/gm x 1.8

gms = 453.6 x lb.

ft³ = gal x .1337

ATM. = Psig x .068

°F = 9/5 °C + 32

HVT lead=.6"

Steam tables also included

MISCELLANEOUS EQUATIONS

$$SUR = \frac{26.0}{\lambda^* + (\beta - \rho) \tau}$$

$$I.d. = I_2 d_2$$

$$I_1 d_1^2 = I_2 d_2^2$$

$$P = P_0 e^{-t/\tau}$$

$$\rho = \frac{\lambda^*}{\tau} + \frac{\beta_{eff}}{1 + \frac{\lambda}{\lambda \tau}}$$

$$R/HR = \frac{.5 CE}{d^2 (\text{meter})}$$

$$CR_1 = \frac{S}{1 - K_{eff,1}}$$

$$\rho = \frac{K-1}{K} = \frac{\Delta K}{K}$$

$$T = \frac{\lambda^*}{\rho} + \frac{\beta - \rho}{\lambda \rho}$$

$$HVL = \frac{0.693}{\mu}$$

$$D.R. = \frac{6CE}{d^2}$$

$$A = \tau r^2$$

$$SUR = \frac{26.06}{\tau}$$

$$PE = mgh$$

$$\tau = \frac{t}{\rho - \beta}$$

$$1 \text{ curie} = 3.7 \times 10^{10} \text{ dps}$$

$$CR_2 = \frac{S}{1 - K_{eff,2}}$$

$$C_1 V_1 + C_2 V_2 + C_{nth} V_{nth} = C_F V_F$$

$$\rho = \frac{\bar{\phi}}{1 + \lambda \tau}$$

$$R_t = \frac{1}{R_1} + \frac{1}{R_2} + \dots + \frac{1}{R_n}$$

$$SDM = \frac{1 - K}{K}$$

$$B = B_0 e^{-Pt/v}$$

$$R_t = R_1 + R_2 + \dots + R_n$$

$$\rho = \frac{1}{\tau K_{eff}} + \frac{\beta}{1 + \lambda \tau}$$

$$M = \frac{CR_2}{CR_1}$$

$$M = \frac{1 - K_{eff,1}}{1 - K_{eff,2}}$$

$$\frac{1}{M} = \frac{1 - K_{eff,1}}{1 - K_{eff,2}}$$

$$\frac{1}{M} = \frac{CR_1}{CR_2}$$

$$\frac{CR_1}{CR_2} = \frac{1 - K_{eff,1}}{1 - K_{eff,2}}$$

Westinghouse

$$\Delta \rho = L_N \frac{K_2}{K_1}$$