40-6659 RETURN TO URFO - DENVER, PDR STACK EMISSIONS SURVEY PETROTOMICS COMPANY URANIUM MILL SHIRLEY BASIN, WYOMING JUNE 1984 FILE NUMBER 8410-136 Prepared By: Western Environmental Services and Testing, Inc. 1403 East Yellowstone Highway Casper, Wyoming 82601 (307) 234-5511 w/etr 8/29/84 01405 8410160085 840829 PDR ADDCK 04006659 C PDR

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STACK EMISSIONS SURVEY
PETROTOMICS COMPANY
URANIUM MILL
SHIRLEY BASIN, WYOMING

INTRODUCTION

Western Environmental Services and Testing, Inc. (WEST, Inc.) of Casper, Wyoming, conducted a Stack Emissions Survey at the Petrotomics Company Uranium Mill located near Shirley Basin, Wyoming, on June 21, 1984. The purpose of this survey was to determine emissions of particulates, Uranium-natural (U), Radium-226, Thorium-230, Lead-210, and Radon-222 from the Yellow Cake Dryer Stack, Packaging Room Exhaust Stack, and Cooler Exhaust Stack.

The sampling followed the procedures set forth in the "Wyoming Air Quality Standards and Regulations," Wyoming Department of Environmental Quality, 1982; the Appendix to the <u>Code of Federal Regulations</u>, Title 40, Chapter I, Part 60; and the United States Nuclear Regulatory Commission <u>Code of Federal Regulations</u>, Title 10, Chapter I, Part 20.

SUMMARY OF RESULTS

The principal conclusions are:

Yellow Cake Dryer Stack

- 1. The emissions of particulate matter from the Yellow Cake Dryer Stack were 0.208 pounds per hour (0.0169 grains per dry standard cubic foot), based on the test using the 'front-half' collections of the EPA-type sampling train.
- 2. The concentration of Uranium-natural (U) was $6.05 \times 10^{-10} \mu \text{Ci/ml}$, based on the test using the 'front-half' collections of the EPA-type sampling train.
- 3. The U_3O_8 emission rate is 0.0056 pounds per hour, based on the test using the 'front-half' collections of the EPA-type sampling train.
- 4. The concentration of Radon gas in the stack gas was 0.9 ± 0.3 pCi/1.

Packaging Room Exhaust Stack

1. The emissions of particulate matter from the Packaging Room Exhaust Stack were 0.055 pounds per hour (0.0114 grains per dry standard cubic foot), based on the test using the 'front-half' collections of the EPA-type sampling train.

- 2. The concentration of Uranium-natural (U) was 2.65×10^{-11} µCi/ml, based on the test using the 'front-half' collections of the EPA-type sampling train.
- 3. The U3Oa emission rate is 0.0010 pounds per hour, based on the test using the 'front-half' collections of the EPA-type sampling train.
- 4. The concentration of Radon gas in the stack gas was 0.1 ± 0.3 pCi/1.

Cooler Exhaust Stack

- The emissions of particulate matter from the Cooler Exhaust Stack were 0.057 pounds per hour (0.0114 grains per dry standard cubic foot), based on the test using the 'front-half' collections of the EPA-type sampling train.
- 2. The concentration of Uranium-natural (U) was $6.52 \times 10^{-9} \, \mu \text{Ci/ml}$, based on the test using the 'front-half' collections of the EPA-type sampling train.
- 3. The $\rm U_3O_8$ emission rate is 0.0248 pounds per hour, based on the test using the 'front-half' collections of the EPA-type sampling train.
- 4. The concentration of Radon gas in the stack gas was 0.1 ± 0.3 pCi/ml.

SUMMARY OF RESULTS

		Yellow Cake	Packaging Room	Cooler Exhaust
Run Number		1	1	1
Stack Flow Rate - ACFM		2366	811	1078
Stack Flow Rate - DSCFM*		1433	566	585 -
% Water Vapor - % Vol.		9.82	3.35	1.29
% CO ₂ - % Vol.		1.4	0.0	0.0
% O ₂ - % Vol.		19.0	21.0	21.0
% Excess Air @ Sampling Point		907		
Particulates Probe, Cyclone & Filter Catch grains/dscf*	(c _{an})	0.0169	0.0114	0.0114
grains/cf @ Stack Conditions	(Cat)	0.0102	0.0079	0.0062
1bs/hr	(Caw)	0.208	0.055	0.057
Total Catch grains/dscf*	(Cao)			
grains/cf @ Stack Conditions	(Cau)			
lbs/hr	(Cax)			
Uranium-natural (U)	Ci/ml	6.05 x 10 ⁻¹⁰	2.65 x 10 ⁻¹¹	6.52 x 10 ⁻⁹
U O Emissions 1	.bs/hr	0.0056	0.0010	0.0248

^{* 68°}F., 29.92 "Hg (20°C, 760 mm Hg)

RADIOCHEMISTRY LABORATORY RESULTS AS REPORTED BY ALPHA ENERGY LABORATORIES, INC. ON AUGUST 27, 1984

YELLOW CAKE DRYER STACK

Sample Date: June 21, 1984

Radon-222* pCi/1 0.9 ± 0.3

LLD - pCi/1 0.2

Uranium-natural (U) µg/seaple 1231

 $\mu gCi/ml$ 6.05 x $10^{-10} \pm 0.02 \times 10^{-10}$

LLD - $\mu \text{Ci/ml}$ 3 x 10⁻¹³

Radium-226

 $\mu \text{Ci/ml}$ 5.61 x 10⁻¹³ ± 2.69 x 10⁻¹³

LLD - $\mu \text{Ci/ml}$ 3 x 10⁻¹³

Thorium-230

 $\mu \text{Ci/ml}$ 2.66 x $10^{-13} \pm 6.35 \times 10^{-13}$

LLD - μ Ci/ml 9 x 10⁻¹²

Lead-210

 $\mu \text{Ci/ml}$ 3.09 x $10^{-12} \pm 3.21 \times 10^{-12}$

LLD - μ Ci/ml 5 x 10⁻¹³

^{*} Radon-222 analyzed by CORE Laboratories.

RADIOCHEMISTRY LABORATORY RESULTS AS REPORTED BY ALPHA ENERGY LABORATORIES, INC. ON AUGUST 27, 1984

PACKAGING ROOM EXHAUST STACK

Sample Date: June 21, 1984

Radon-222* pCi/1 0.1 ± 0.3

LLD - pCi/1 0.2

Uranium-natural (U) µg/sample 32.4

 $\mu gCi/ml$ 2.65 x $10^{-11} \pm 0.03 \times 10^{-13}$

LLD - μ Ci/ml 4 x 10⁻¹³

Radium-226

 $\mu \text{Ci/ml}$ 1.58 x $10^{-12} \pm 0.74 \times 10^{-12}$

LLD - $\mu \text{Ci/ml}$ 9 x 10⁻¹³

Thorium-230

 $\mu \text{Ci/ml}$ 4.28 x $10^{-13} \pm 33.4 \times 10^{-13}$

LLD - μ Ci/ml 5 x 10⁻¹²

Lead-210

 $\mu \text{Ci/ml}$ 0.0 ± 7.34 x 10⁻¹²

LLD - μ Ci/ml 1 x 10⁻¹²

^{*} Radon-222 analyzed by CORE Laboratories.

RADIOCHEMISTRY LABORATORY RESULTS AS REPORTED BY ALPHA ENERGY LABORATORIES, INC. ON AUGUST 27, 1984

COOLER EXHAUST STACK

Sample Date: June 21, 1984

Radon-222* pCi/1

pCi/1 0.1 ± 0.3

LLD - pCi/1 0.2

Uranium-natural (U) µg/sample 13984

 μ gCi/ml 6.52 x 10⁻⁹ ± 0.02 x 10⁻⁹

LLD - μ Ci/ml 2 x 10⁻¹³

Radium-226

 $\mu \text{Ci/ml}$ 8.81 x $10^{-13} \pm 4.32 \times 10^{-13}$

LLD - μ Ci/ml 6 x 10⁻¹³

Thorium-230

 $\mu \text{Ci/ml}$ 9.59 x $10^{-12} \pm 3.47 \times 10^{-12}$

LLD - μ Ci/ml 4 x 10⁻¹²

Lead-210

 $\mu \text{Ci/ml}$ 5.76 x $10^{-12} \pm 3.38 \times 10^{-12}$

LLD - μ Ci/ml 5 x 10⁻¹³

^{*} Radon-222 analyzed by CORE Laboratories.

RADON-222 RESULTS

Sample Date: June 21, 1984

Yellow Cake Dryer Stack	pCi/1	0.9 ± 0.3
	LLD - pCi/1	0.2
Packaging Room Exhaust Stack	pCi/l	0.1 ± 0.3
	LLD - pCi/1	0.2
Cooler Exhaust Stack	pCi/l	0.1 ± 0.3
	LLD - pCi/1	0.2

DISCUSSION OF RESULTS

The one test for particulates taken on each stack appeared to be valid representations of the actual emissions. The indicative parameters calculated from the field data were in close agreement to previous tests. The rates of sampling for the tests on the Packaging Room Exhaust Stack and the Cooler Exhaust Stack were well within the specified limits of the isokinetic rate. The rates of sampling for the test on the Yellow Cake Dryer Stack were lower than the specified limits, the greatest deviation being 15.59 percent. However, based on previous experience, WEST, Inc. feels that the particulate values were not biased greatly and do represent the actual emissions.

DESCRIPTION OF PROCESS OPERATION

In a uranium milling operation, uranium is extracted from ore, purified, and converted to $\rm U_3O_8$. The raw ore is crushed and mixed with sulfuric acid to leach out the uranium. The mixture goes through a sand-slime separation to remove and wash the sand. The de-sanded pulp is collected and transferred to the resin-in-pulp circuit where ion-exchange resin is removed counter-current to the solution flow.

This mixture goes to the clarifier where a filter removes solids and routes the pregnant solution to the solvent extraction circuit. The uranium-sulfuric acid mixture is removed from the organic phase by ammonium sulfate. The solution then goes to a precipitation tank where yellow cake is precipitated upon addition of ammonia. The yellow cake is dried, converted to U_3O_8 , and conveyed to a storage hopper where it is loaded into 55-gallon drums for shipment.

DESCRIPTION OF SAMPLING LOCATIONS

Yellow Cake Dryer Stack

The sampling ports on the Yellow Cake Dryer Stack are located approximately 35 feet above the ground. The sampling was performed from two ports on the circular stack located approximately 10 feet (10.0 stack diameters) downstream from the stack inlet and approximately 2 feet (2.0 stack diameters) upstream from the stack outlet.

Packaging Room Exhaust Stack

The sampling ports on the Packaging Room Exhaust Stack are located approximately 35 feet above the ground. The sampling was performed from two ports on the circular stack located approximately 8 feet 11 inches (10.44 stack diameters) downstream from the stack inlet and approximately 4 feet 1 inch (4.78 stack diameters) upstream from the stack outlet.

Cooler Exhaust Stack

The sampling ports on the Cooler Exhaust Stack are located approximately 35 feet above the ground. The sampling was performed from two ports on the circular stack located approximately 5 feet 10 inches (4.5 stack diameters) downstream from the stack inlet and approximately 3 feet (2.3 stack diameters) upstream of the stack outlet.

SAMPLING AND ANALYTICAL PROCEDURES

The sampling and analytical procedures used followed the procedures set forth in the "Wyoming Air Quality Standards and Regulations", Wyoming Department of Environmental Quality, 1982; the Appendix to the Code of Federal Regulations, Title 40, Chapter I, Part 60; and the United States Nuclear Regulatory Commission, Code of Federal Regulations, Title 10, Chapter I, Part 20.

A preliminary velocity traverse was made at each port in order to determine the uniformity of flow in the Yellow Cake Dryer Stack. Particulate samples of 5-minute duration at each of the six traverse points were taken from each port using an EPA-type, heated, glass-lined probe. The first and sixth points were not sampled because they were less than 1 inch from the stack wall. Instead, points 2 and 5 were sampled twice.

A preliminary velocity traverse was made at each port in both the Packaging Room Exhaust and Cooler Exhaust Stacks. Particulate samples of 5-minute duration at each of the six traverse points were taken from each port on the Packaging Room Exhaust Stack. Particulate samples of 3-minute duration at each of the 12 traverse points were taken from each port on the Cooler

Exhaust Stack. All samples taken from the Packaging Room Exhaust and Cooler Exhaust Stacks utilized an EPA-type, heated, glass-lined probe.

Before the test, the sampling train was leak-checked at 15 inches of mercury. After the test, the train was again leak-checked at the highest recorded vacuum reading during the test. Final leak-checking was performed in order to predetermine the possibility of a diluted sample.

Before and after each test, the pitot tube lines were checked for leaks under both a vacuum and pressure; the lines were checked for clearance; and the zero manometer reading verified.

The emissions were calculated from gravimetric analysis using the 'front-half' collections of the EPA-type sampling train. The 'front-half' particulate and filters were analyzed by Alpha Energy Laboratories, Inc., Dallas, Texas.

DESCRIPTION OF TESTS

Personnel from WEST, Inc. arrived at the Petrotomics Company Uranium Mill near Shirley Basin, Wyoming, at 0800 hours on Thursday, June 21, 1984.

The sampling equipment was moved onto the Yellow Cake Dryer Stack and prepared for testing by 0845 hours. Testing began at 0851 hours and was completed by 0954 hours.

The equipment was moved onto the Packaging Room Exhaust Stack. Testing began at 1034 hours and continued until completion at 1137 hours. The equipment was moved onto the Cooler Exhaust Stack. Testing began at 1218 hours and continued until completion at 1321 hours. Radon-222 gas samples were taken from each stack during the test.

The equipment was moved off the stack and loaded into the mobile laboratory.

The samples were recovered and taken to WEST, Inc.'s laboratory in Casper,

Wyoming, for further analyses and evaluation.

Testing at Petrotomics Company's Uranium Mill was completed at 1400 hours on Thursday, June 21, 1984.

Brace A. Hinchey

President

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APPENDICES

- A. Location of Sampling Points
- B. Source Emission Calculations
- C. Calibration of Equipment
- D. Field Testing Data
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- G. Resumes of Test Personnel

APPENDIX A

Location of Sampling Points

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Location of Sampling Points

Yellow Cake Dryer Stack

The sampling ports are located approximately 10 feet (10.0 stack diameters) downstream from the stack inlet and approximately 2 feet (2.0 stack diameters) upstream of the stack outlet. The first and sixth sample points were not sampled because they were less than one inch from the stack wall; instead, points two and five were double sampled. The locations of the sampling points were calculated as follows:

Inside Stack Diameter = 12 inches

Port and Wall Thickness = 4 inches

Point No.	Percent of Diameter From Wall	Distance From Wall
1	4.4	
2	14.7	1-3/4"
3	29.5	3-1/2"
4	70.5	8-1/2"
5	85.3	10-1/4"
6	95.6	

Packaging Room Exhaust Stack

The sampling ports are located approximately 8 feet 11 inches (10.44 stack diameters) downstream from the stack inlet and approximately 4 feet 1 inch (4.78 stack diameters) upstream from the stack outlet. The locations of the sampling points were calculated as follows:

Inside Stack Diameter = 10-1/4 inches

Port and Wall Thickness = 4-1/2 inches

Point No.	Percent of Diameter From Wall	Distance From Wall
1*	4.4	1/2"
2	14.7	1-1/2"
3	29.5	3"
4	70.5	7-1/4"
5	85.3	8-3/4"
6*	95.6	9-3/4"

^{*} Points 1 and 6 were adjusted to within 1/2" due to their proximity to the stack wall.

Cooler Exhaust Stack

The sampling ports are located approximately 5 feet 10 inches (4.5 stack diameters) downstream from the stack inlet and approximately 3 feet (2.3 stack diameters) upstream of the stack outlet. The first and twelfth points were not sampled because they were less than one inch from the stack wall; instead, points two and eleven were double sampled. The locations of the sampling points were calculated as follow:

Inside Stack Diameter = 15 1/2 inches

Port and Wall Thickness = 4 1/2 inches

Point No.	Percent of Diameter From Wall	Distance From Wall
1	2.1	L
2	6.7	1"
3	11.8	1 13/16"
4	17.7	2 3/4"
5	25.0	3 7/8"
6	35.5	5 1/2"
7	64.5	10"
8	75.0	11 5/8"
9	82.3	12 3/4"
10	88.2	13 11/16"
11	93.3	14 1/2"
12	97.9	

APPENDIX B

Nomenclature and Equations for Calculation of Source Emissions

Nomenclature for Particulate Calculations

Symbol Symbol	English Units	Metric Units	Description
As	in. ²	m ²	Stack Area
c _{an}	gr/dscf	g/dscm	Particulate - Probe, Cyclone and Filter
c _{ao}	gr/dscf .	g/dscm	Particulate - Total
Cat	gr/CF @ Stack Conditions	g/m³	Particulate - Probe, Cyclone and Filter
Cau	gr/CF @ Stack Conditions	g/m³	Particulate - Total
Caw	lbs/hr	kg/hr	Particulate - Probe, Cyclone and Filter
C _{ax}	lbs/hr	kg/hr	Particulate - Total
C _p			Pitot Tube Calibration Factor
D _n	in.	m	Sampling Nozzle Diameter
%EA			Percent Excess Air At Sampling Point
g	32.2 ft/sec ²		Acceleration Of Gravity
21			Percent Isokinetic
2M			Percent Moisture In The Stack Gas By Volume

^{* 528°}R, 29.92 "Hg (20°C, 760 mm Hg)

Symbol Symbol	English Units	Metric Units	Description
M _d			Mole Fraction of Dry Gas
mf	mg	mg	Particulate - Probe, Cyclone and Filter
M _{H2O}	18 1b/1b-mole		Molecular Weight Of Water
m _t	mg	mg	Particulate - Total
MWair	lb/lb-mole	g/g-mole	Molecular Weight Of Stack Gas
MW	28.95 1b/ 1b-mole		Molecular Weight Of Air
MW _d	1b/1b-mole	g/g-mole	Molecular Weight Of Dry Stack Gas
P _b	"Hg Absolute	mm Hg	Barometric Pressure
P _m	"H ₂ 0	mm H ₂ O	Orifice Pressure Drop
Ps	"Hg		
5	Absolute	mm Hg	Stack Pressure
ΔPs	"H ₂ O	mm H ₂ O	Velocity Head Of Stack Gas
Pstd	29.92 "Hg	760 mm Hg	Standard Barometric Pressure
Q _a	ACFM	m ³ /hr	Stack Gas Volume At Actual Stack Conditions
Qs	DSCFM	dscm/hr	Stack Gas Volume At 29.92 "Hg, 528°R, Dry
R	21.83 "Hg- ft ³ /lb-mole-°R		Universal Gas Constant
* 528°R, 2	9.92 "Hg (20°C, 7	60 mm Hg)	

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Symbol Symbol	English Units	Metric Units	Description
T _m	°F	°c	Average Gas Meter Temperature
T _t	min	min	Net Time Of Test
Ts	°F	°c	Stack Temperature
T _{std}	528°R	293°K	Standard Temperature
V _m	ft ³	m ³	Volume Of Dry Gas Sampled @ Meter Conditions
V _m std	dscf	dscm	Volume Of Dry Gas Sampled @ Standard Conditions
V _s	fpm	m/sec	Stack Velocity @ Stack Conditions
V _w	ml	ml	Total Water Collected In Impingers And Silica Gel
V wgas	scf	scm	Volume Of Water Vapor Collected @ Standard Conditions
Pair	0.0748 lbs/ft ³		Density Of Air
^р н ₂ о	. 1 g/ml		Density Of Water
oman	51.63 lbs/ft ³		Density Of Manometer Oil
	Standard Condit	ions: 68°F,	29.92 "Hg (20°C, 760 mm Hg)

Example Particulate Calculations

1. Volume Of Dry Gas Sampled At Standard Conditions.*

$$V_{m_{std}} = V_{m} \left[\frac{T_{std}}{T_{m} + 460} \right] \left[\frac{P_{b} + \frac{P_{m}}{13.6}}{P_{std}} \right]$$

$$V_{m_{std}} = 17.65 V_{m} \left[\frac{P_{b} + \frac{P_{m}}{13.6}}{T_{m} + 460} \right] = dscf$$

$$V_{m} = dscf \times 0.028317 = dscm$$

2. Volume Of Water Vapor Collected At Standard Conditions.*

$$V_{\text{gas}} = \frac{(V_{\text{W}} - \text{gms } SO_2 - \text{gms } H_2S) \rho_{H_2O} R T_{\text{std}}}{P_{\text{std}} M_{H_2O} 453.6}$$

$$V_{\text{wgas}} = 0.0472 (V_{\text{w}} - \text{gms SO}_2 - \text{gms H}_2\text{S}) = \text{scf}$$

$$V_{\text{wgas}} = \text{scf} \times 0.028317 = \text{scm}$$

3. Percent Moisture In Stack Gas.

$$%M = \frac{V_{\text{wgas}}}{V_{\text{mstd}} + V_{\text{wgas}}} \times 100 = %$$

* 528°R, 29.92 "Hg (20°C, 760 mm Hg)

4. Mole Fraction Of Dry Gas.

$$M_d = \frac{100 - %M}{100}$$

5. Average Molecular Weight Of Dry Stack Gas.

$$MW_{d} = \left(\%CO_{2} \times \frac{44}{100} \right) + \left(\%O_{2} \times \frac{32}{100} \right) + \left(\%N_{2} \times \frac{28}{100} \right) + \left(\%CO \times \frac{28}{100} \right) = 1b/1b-mole = g/g-mole$$

6. Molecular Weight Of Stack Gas.

$$MW = MW_d \times M_d + 18 (1-M_d) = \frac{1b}{1b-mole} = g/g-mole$$

7. Percent Excess Air At Sampling Point.

%EA =
$$\frac{100 (\%0_2 - 0.5\% \text{ CO})}{0.265 (\%N_2) - (\%0_2) + 0.5 (\%\text{CO})}$$

8. Stack Pressure.

$$P_s = P_b + \frac{\text{stack pressure "}H_2O}{13.6} = \text{"Hg Absolute}$$

$$P_s = \text{"Hg Abs. x 25.4} = \text{mm Hg}$$

* 528°R, 29.92 "Hg (20°C, 760 mm Hg)

9. Stack Velocity At Stack Conditions.

$$V_{s} = C_{p} 60 \left[\frac{2g \times \rho_{man} \times P_{std} \times MW_{air} \times (T_{s} + 460) \times \Delta P_{s}}{12 \times \rho_{air} \times P_{s} \times MW \times T_{std}} \right] 1/2$$

$$V_{s} = 5123.8 C_{p} \left[\frac{(T_{s} + 460)}{P_{s} \times MW} \right]^{\frac{1}{2}} \times Average \left[(\Delta P)^{\frac{1}{2}} \right] = fpm$$

 $V_s = fpm \times 0.00508 = m/sec$

10. Dry Stack Gas Volume At Standard Conditions.*

$$Q_{s} = \frac{1}{144} V_{s} \times A_{s} \times M_{d} \times \frac{T_{std}}{T_{s} + 460} \times \frac{P_{s}}{P_{std}}$$

$$Q_{s} = \frac{0.123 \text{ V}_{s} \times A_{s} \times M_{d} \times P_{s}}{T_{s} + 460} = DSCFM$$

$$Q_s = DSCFM \times 1.6990 = dscm/hr$$

11. Actual Stack Gas Volume At Stack Conditions.

$$Q_a = \frac{V_s \times A_s}{144} = ACFM$$

$$Q_n = ACFM \times 1.6990 = m^3/hr$$

12. Percent Isokinetic.

13. Particulate - Probe, Cyclone, and Filter.

$$C_{an} = \frac{m_f}{V_{m_{std}}} \times \frac{1 \text{ gr}}{64.8 \text{ mg}}$$

$$C_{an} = 0.0154 \quad \frac{m_f}{V_{m_{std}}} = \text{gr/dscf}$$

$$C_{an} = gr/dscf \times 2.290 = g/dscm$$

14. Particulate - Total.

$$C_{ao} = 0.0154 \times \frac{m_t}{V_{m_{std}}} = gr/dscf$$

$$C_{ao} = gr/dscf \times 2.290 = g/dscm$$

15. Particulate - Probe, Cyclone, and Filter At Stack Conditions.

$$C_{at} = C_{an} \times \frac{P_{s}}{P_{std}} \times \frac{(T_{std})}{(T_{std} + 460)} \times M_{d}$$

$$C_{at} = \frac{17.65 \times C_{an} \times P_{s} \times M_{d}}{T_{s} + 460} = gr/CF$$

$$C_{at} = gr/CF \times 2.290 = g/m^3$$

16. Particulate - Total, At Stack Conditions.

$$C_{1} = \frac{17.65 \times C_{ao} \times P_{s} \times M_{d}}{T_{s} + 460} = gr/CF$$

$$C_{au} = gr/CF \times 2.290 = g/m^3$$

17. Particulate - Probe, Cyclone, and Filter.

$$C_{aw} = C_{an} \times Q_{s} \times \frac{60 \text{ min}}{1 \text{ hr}} \times \frac{1 \text{ lb}}{7000 \text{ gr}}$$

$$C_{aw} = 0.00857 \times C_{an} \times Q_{s} = 1bs/hr$$

$$C_{aw} = 1bs/hr \times 0.4536 = kg/hr$$

18. Particulate - Total.

$$C_{ax} = 0.00857 \times C_{ao} \times Q_{s} = 1bs/hr$$

$$C_{ax} = 1bs/hr \times 0.4536 = kg/hr$$

* 528°R, 29.92 "Hg (20°C, 760 mm Hg)

Uranium Calculations

[$\mu g U / V m s t d (m^3)$] [1 X $10^{-6} m^3 / m l$] = $\mu g U / m l$ [$\mu g U / m l$] [6.77 X $10^{-7} \mu C i / \mu g$] = $\mu C i / m l$ Uranium

Ra²²⁶ Calculations

[pCi Ra²²⁶/Vmstd (m³)] [1 X 10⁻⁶ m³/ml] = pCi/ml Ra²²⁶ [pCi Ra²²⁶/ml] [1 X 10⁻⁶ μ Ci/pCi] = μ Ci/ml Ra²²⁶

Th²³⁰ Calculations

[pCi Th²³⁰/Vmstd (m³)] [1 X 10⁻⁶ m³/ml] = pCi/ml Th²³⁰ [pCi Th²³⁰/ml] [1 X 10⁻⁶ μ Ci/pCi] = μ Ci/ml Th²³⁰

Pb²¹⁰ Calculations

[pCi Pb²¹⁰/Vmstd (m³)] [1 X 10⁻⁶ m³/ml] = pCi/ml Pb²¹⁰ [pCi Pb²¹⁰/ml] [1 X 10⁻⁶ μ Ci/pCi] = μ Ci/ml Pb²¹⁰

U308 Pound Per Hour

 $\frac{\mu g U}{\text{Sample}} \times (1 \times 10^{-3}) \times 1.1792731 \frac{\text{mg } U_3 O_8}{\text{mg } U-\text{Nat}} \times 0.0154 = \text{grains/dscf}$

 $\frac{\text{grains}}{\text{dscf}}$ X 0.00857 X $\frac{\text{DSCF}}{\text{Minute}}$ = U₃O₈ lbs/hour

PETROTOMICS COMPANY
URANIUM MILL
SHIRLEY BASIN, WYOMING

JUNE 1984

FILE NUMBER 8410-136

SOURCE EMISSION CALCULATIONS

Symbol	Description	Units	PKG EXHAUST	YCD
Run No.			1	1
Date			6/21/84	6/21/84
Begin			1034 MST	0851 MST
End			1137 MST	0954 MST
P _b	barometri pressure	"Hg Abs. (mm Hg)	23.30 591.82	23.20 589.28
P _m	orifice pressure drop	"H ₂ 0 (mm H ₂ 0)	0.89 22.52	2.56 64.98
V _m	volume dry gas sampled a meter conditions	ft. ³ (m ³)	37.996 1.076	62.648 1.774
T _m	avg. gas meter temp	°F (°C)	76 24	72 22
mstd	volume dry gas sampled @ standard conditions*	dsef (dscm)	29.248 .828	48.611 1.377
V _w	total H ₂ O collected, impingers & silica gel	ml	21.5	112.2
V wgas	volume water vapor collected @ standard conditions*	scf (scm)	1.015	5.296 .15
ZM	moisture in stack gas by volume	%	3.35	9.82

^{* 68°}F, 29.92 "Hg (20°C, 760 mm Hg)

Symbol	Description	Units	PKG EXHAUST	YCD 1
M _d	mol fraction of dry gas		.9665	.9018
co ₂		%	0	1.4
02		%	21	19
N ₂		X	79	79.6
%EA	excess air @ sampling point	%		907
MW _d	molecular weight of dry stack gas	1b/lb-mole (g/g-mole)	28.84 28.84	28.98 28.98
MW	molecular weight of stack gas	1b/15-mole (g/g-mole)	28.48 28.48	27.91 27.91
ΔPs	velocity head of stack gas	"H ₂ 0 (mm H ₂ 0)	.134 3.40	.548 13.92
T _s	stack temperature	°F (°C)	112 45	152 67
Ps	stack pressure	"Hg Abs. (mm Hg)	23.30 591.91	23.21 589.43
V _s	stack velocity @ stack conditions	fpm (m/sec)	1424 7.24	3015 15.32
As	stack area	in. ² (m ²)	82 0.05	113 0.07
Qs	dry stack volume @ standard conditions*	DSCFM (dscm/hr)	566 960.83	1433 2434.86
Q _a	actual stack gas volume @ stack conditions	ACFM (m ³ /hr)	811 1378.08	2366 4019.66

Symbol Symbol	Description	Units	PKG EXHAUST	YCD 1
Tt	net time of test	unin.	60	60
D _n	sampling nozzle diam.	in. (m)	.311	.311
71	percent isokinetic	%	93.39	84.41
m _F	particulate - probe, cyclone and filter	mg,	21.7	53.4
m _c	particulate - total	mg		
C _{an}	particulate - probe, cyclone and filter	gr/dscf* (g/dscm)	.0114	.0169 .0387
C _{ao}	particulate - total	gr/dscf* (g/dscm)	. g ===	/==
c _{at}	particulate - probe, cyclone and filter @ stack conditions	gr/cf (g/m ³)	.0079	.0102 .0234
c _{au}	particulate total @ stack conditions	gr/cf (g/m ³)	===	
¢ _{aw}	particulate - probe, cyclone and filter	lbs/hr (kg/hr)	.055 .025	.208
c,	particulate - total	lbs/hr (kg/hr)	19	1

^{# 68°}F, 29.92 "Hg (20°C, 760 mm Hg)

STACK EMISSIONS SURVEY PETROTOMICS COMPANY URANIUM MILL SHIRLEY BASIN, WYOMING

JUNE 1984

FILE NUMBER 8410-136

SOURCE EMISSION CALCULATIONS

Symbol	Description	Units	COOLER EXH.
Run No.			1
Dace			6/21/84
Begin			1218 MST
End			1321 MST
P _b	barometric pressure	"Hg Abs. (mm Hg)	23.30 591.82
P _m	orifice pressure drop	"H ₂ 0 (mm H ₂ 0)	0.00
V _m	volume dry gas sampled @ meter conditions	ft. ³ (m ³)	67.729 1.918
T _m	avg. gas meter temp	°F (°C)	83 28
V _m std	volume dry gas sampled @ standard conditions*	dscf (dscm)	51.277 1.452
V _w	total H ₂ O collected, impingers & silica gel	ml	14.2
v _w gas	volume water vapor collected @ standard conditions*	scf (scm)	.67 .619
%M	moisture in stack gas by volume	%	1.29

Symbol Symbol	Description	Units	COOLER EXH
M _d	mol fraction of dry gas		.9871
co ₂		%	0
02		76	21
N ₂		%	79
%EA	excess air @ sampling point	%	
MWd	molecular weight of dry stack gas	1b/1b-mole (g/g-mole)	28.84 28.84
MW	molecular weight of stack gas	1b/lb-mole (g/g-mole)	28.70 28.70
ΔΡs	velocity head of stack gas	"H ₂ 0 (mm H ₂ 0)	.037 0.94
T _s	stack temperature	°F (°C)	291 144
Ps	stack pressure	"Hg Abs. (mm Hg)	23.30 591.75
Vs	stack velocity @ stack conditions	fpm (m/sec)	822 4.17
A _s	stack area	in. ² (m ²)	189 0.12
Qs	dry stack volume @ standard conditions*	DSCFM (dscm/hr)	585 994.17
^Q a	actual stack gas volume @ stack conditions	ACFM (m ³ /hr)	1078 1831.91

Symbol Symbol	Description	Units	COOLER EXH
T _t	net time of test	mín.	60
D _n	sampling nozzle diam.	in. (m)	.612 .016
%I	percent isokinetic	%	94.19
m _f	particulate - probe, cyclone and filter	mg	37.8
m _C	particulate - total	mg	
C _{an}	particulate - probe, cyclone and filter	gr/dscf* (g/dscm)	.0114
C _{ao}	particulate - total	gr/dscf* (g/dscm)	===
Cat	particulate - probe, cyclone and filter @ stack conditions	gr/cf (g/m ³)	.0062 .0142
c _{au}	particulate total @ stack conditions	gr/cf (g/m ³)	
Caw	particulate - probe, cyclone and filter	lbs/hr (kg/hr)	.057 .026
c _{ax}	particulate - total	lbs/hr (kg/hr)	111

^{* 68°}F, 29.92 "Hg (20°C, 760 mm Hg)

APPENDIX C

Calibration of Equipment

APPENDIX C

Calibration Data

June 4, 1984

NOZZLES

Se	t #A	Se	t #B
Nozzle No.	Diameter (inches)	Nozzle No.	Diameter (inches)
		1B	0.128
		2B	0.176
3A	0.254	3B	0.241
4A	0.318	4B	0.300
5A	0.354	5B	0.359
6A	0.377		
7A	0.448	7B	0.500
8A	0.493		0.500
9A	0.499		
10A	0.576		

Set	I	Set	II	Set	III
Nozzle No.	Diameter (inches)	Nozzle	Diameter (inches)	Nozzle	Diame (inch

Nozzle No.	(inches)	Nozzle No.	Diameter (inches)	Nozzle No.	Diameter (inches)
I-1	0.131	II-1	0.123	III-l	0.127
I-2	0.196	II-2	0.197		
I-3	0.245	II-3	0.249	III-3	0.247
I-4	0.310	II-4	0.311	III-4	0.373
I-5	0.373	II-5	0.374	III-5	0.365
I-6	0.419	II-6	0.430	III-6	0.437
I-7	0.490	11-7	0.498	III-7	0.499
I-8	0.571	II-8	0.555	III-8	0.566
1-9	0.616	II-9	0.612	III-9	0.613

APPENDIX C

Calibration Data

June 4, 1984

PITOT TUBES

Pitot Length (effective length)	Calibrat	ion Factor
32-1	High	0.818
	Low	0.820
46-1	High	0.824
	Low	0.824
49-1	High	0.823
	Low	0.831
72-1	High	0.832
	Low	0.826
73-1	High	0.829
	Low	0.836
74-1	High	0.828
	Low	0.836
96-1	High	0.823
	Low	0.824
128-1	High	0.826
	Low	0.828
129-1	High	0.825
	Low	0.826
132-1	High	0.833
	Low	0.832
156-1	High	0.824
	Low	0.823
156-2	High	0.831
	Low	0.831

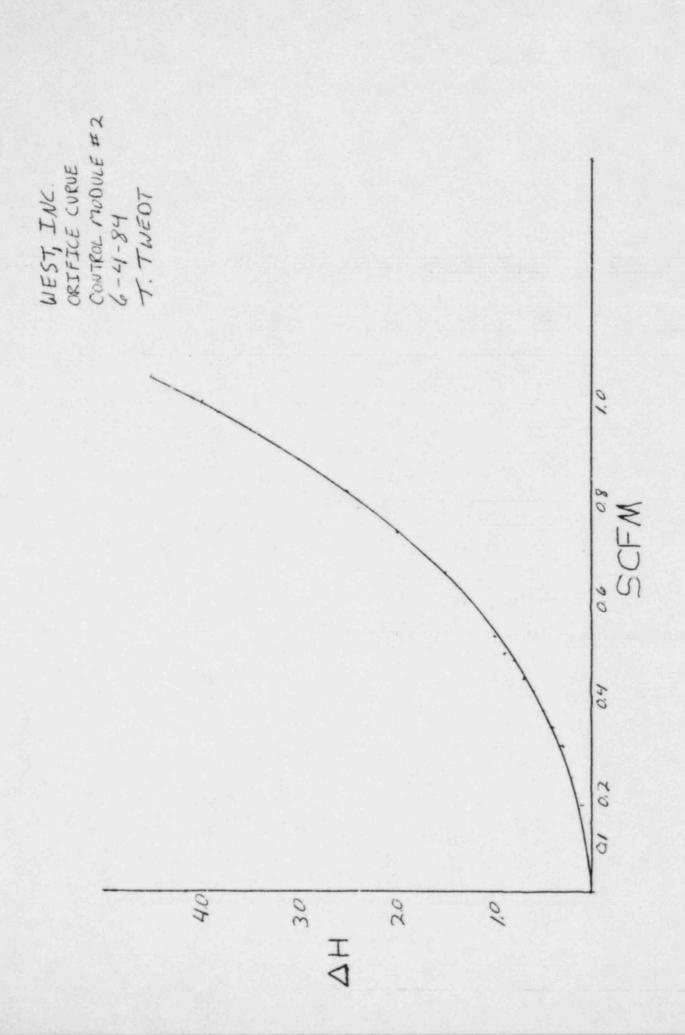
APPENDIX C

Calibration Data

June 4, 1984

DRY GAS METERS

Unit Number	Calibration Factor
1	1.034
2	1.037
3	1.021
4	0.990



APPENDIX D

Field Testing Data

-				-		-		6038 6			ma		
Job N	0	3410-136	2	-	11	7, 4, 6,05	FIELD	DATA	Nomogi	raph Setting	AP O	45 MI 0	2.10
Job N	ame/	e trotames	\$	-					Ambier	nt Temp. °F	60	-	
Run N	0.	/							Assume	d Moisture	% 22		
Locat	ion /	VCD			Application and the second second	d and Reco	THE RESERVE OF THE PERSON NAMED IN COLUMN 2 IN COLUMN	The state of the s	Probe	Length 3	7 1		
		11-84			Sta	rt of Each	n Test P	oint.	Pitot	Tube Leak C	heck B	al ste	Asky IL
			,							l Leak @			
		wchy- 6			2						,		
Sample	e Box No		Meter b	Box No.	Pm		Ts		Final	Leak @	10	Tm = C/C	occ cim
Point	Clock	Dry Gas	Pitot	Orifi	lce ΔH	Pump Vacuum	Stack Temp	Probe	Oven	Effluent Temp	Dry G	as Temp	Remarks
Torne	Time	Meter, CF	in. H ₂ 0		H ₂ O	In. Hg	°F	Temp	Temp	°F			Remarks
1	8.51	12,200	0.51	Desired	Actual	Gauge	151	230	100	64	Inlet	Outlet	
4-5	856	317.12	0.54	2050	2050	6.5	151	233	267	5 9	69	67	
4	901	322.00	0.56	2,60	2-60	6.5	152	235	265	58	70	67	
3	06	327.05	0.56	2.60	2-60	7.0	152	740	228	61	72	67	
2	11	332.32	0.54	2050	2.50	7.0	151	732	268	66	74	67	
1	16	337.08	0,54		2-50	7.0	151	233	264	71	76	68	
END	931	342-078	_		-		-	_	-	_		-	
B-6	924	3471078	0.54	2.50	3-50	70	153	233	761	70	75	68	
5	79	347.52	0.58	12070	2.70	7,0	153	237	269	66	78	68	
3	34	352.55	0.60	2.80	2.80	7:5	153	238	264	64	80	69	
	39	357.55	0.56	2-60	2.60	7.0	153	236	259	65	81		
2	44	362-76	0.54	2.50	2.50	2-0	151	237	358	66	83	70	
	954	368-20	0.51	2.45	2-45	6.0	152	238	252	66	84	70	
END ALL	157	372,613					****						
111													
Volume	Collecte	bration Factor	/6 ft ³	%C0	2 1-4	%co <u>0-0</u>	2_			Initial			
		vw //2.		127		%N2 79		= Dry Ga Calibr	ation F	actor /10	37 X	60.413	
		- 6		Sta	o.k	2 _1/3	1	Dry Ga	Reading	ft	-(Tt	min x Lea	ak ctm)
Baro. P	ress. P _b	23.7	— "Hg	Pre	ss. +0,	08 in.	Н20	Mr	= <	3,4	Mr. =		
							1	F					

	, ,,,,,			
SAMPLE NO.: _	1- 1CD			
IMPINGER NO.	SOLUTION USED	AMOUNT OF SOLUTION (ml)	IMP. TIP CONFIGURATION	WEIGHT (grams)
1	PF HOO	100	_ W 00	Final 593/3 Initial 590:3 Wt. Gain 53.0
2	DI-HOO	100	5. Greenburg	Final 590/8 Initial 56/9 Wt. Gain 28/9
3	DAY		MOD	Final 469-4 Initial 459.5 Wt. Gain 99
4	Gilica Gel		4 010	Final 807-1 Initial 786-7
5				FinalInitial
6				Wt. Gain Final Initial Wt. Gain
Flask				Final
TOTAL WEIGH	T GAIN OF IMPINGER	RS (grams)//a	1.2	
			DATE: 6-3	11-84
		SI	GNATURE:	alles
		SAT ANALYSIS RESU		
		Gas Fractional Pa	irt	
		114		
		19.0		
		010		
	N ₂ -	79.6	-	
SIGNATURE:	18 1.	0//	DATE: _ 6-21-	84
	The state of		TIME: 1000	<u> </u>

Job N Run N Locat	ame <u>le</u>	10-136 Tretomics CK-FKh			Read	and Record of Each	ord at th	he	Ambien Assume Probe	aph Setting t Temp. °F d Moisture Length Tube Leak C	% 10 32°		.,
Opera	tor H	uchey 1			Pm		Ts		Initia Final	1 Leak @	15	"Hg = 92" "Hg = 92" Tm	boo cfm
Point	Clock Time	Dry Gas Meter, CF	Pitot in. H ₂ O	Orifi in.	Н20	Pump Vacuum In. Hg	Stack Temp °F	Probe Temp °F	Oven Temp	Effluent Temp °F		as Temp	Remarks
A-6 5 4 3 2 1 END 8-6 5 4 3 END A-1	1034 34 44 49 54 1107 1107 12 17 22 31 1137	379.37 382-51 385-60 388-80 391-566 391-566 594.50 397-10 403.72 403.72 406.90	0.13 0.13 0.13 0.13 0.13 0.13 0.13 0.14 0.14 0.14	Desired 0.80 0.89 0.86 0.86 0.86 0.86 0.86 0.92 0.92 0.92	Actual 0.80 0.99 0.99 0.86 0.86 0.80 0.80 0.80 0.80	Gauge 3.0 3.0 3.0 3.0 3.0 3.0 3.0 3.0 3.0	110	231 232 232 236 228 238 239 246 251 246 246	256 246 267 264 265 766 862 260 261 260 261	55 59 50 48 48 48 79 58 50 50 51 51	Inlet 23 24 27 28 29 29 29 29 30 81 82 83	Outlet 7/ 7/ 7/ 72 72 73 73 23 24 74 74 74	
Volume Water C	Collected ollected Test T _t	bration Factor by 37,9, 21-5	96 ft ³ m1min	%C0 %O ₂ Are	a Stack A	$\frac{1}{10.32}$ $\frac{32}{2000}$ $\frac{32}{200}$ \frac	O V _n	Probe = Dry Ga Calibr	Tip No.	InitialP actor [-0]	robe Tip	Dia. O	.3// in

SAMPLE NO.: _	1- PACK. FXI	4		
IMPINGER NO.	SOLUTION USED	AMOUNT OF SOLUTION (ml)	IMP. TIP CONFIGURATION	WEIGHT (grams)
1	DI-H20	100	4115	Final 555.0 Initial 542-6 Wt. Gain 12.4
2	DF-H20	100	S. Green buy	Final 570.0 Initial 567.7 Wt. Gain 2-3
3	DRY		mon	Final 494-7 Initial 493.2 Wt. Gain 1.5
4	5, 1, cotal		moo	Final 890-9 Initial 885.6 Wt. Gain 5-3
5				FinalInitialWt. Gain
6				Final Initial Wt. Gain
Flask				Final Initial Wt. Gain
TOTAL WEIG	HT GAIN OF IMPINGER	S (grams)	71.5	
		SI	DATE: 6-2	1-84 19/4/
	OF	SAT ANALYSIS RESU	JLTS	
		Gas Fractional Pa	irt 1	
	co ₂ _		_ VI.	10
	02 -			
	со_		/	
	N ₂ -			
SIGNATURE:	But!	Musty	DATE: 6-2/-	84
	,,		TIME:	

Job N	0. 8	410-136			1/2	f-4:03	FIELD	DATA	Nomogr	aph Setting	AP O	019 AH	1,50
Job N	ame f	Tro 7200	1105		,		_			t Temp. °F			
		/									9 3		
		00/ac 2			Read	d and Reco	ord at	the	Probe Length 33"				
			261	Martine Martin		rt of Each			Probe	Length	20	-,,	16 1
		21-84							Pitot	Tube Leak C	heck 78	4 4	a see
Opera	tor _/-	tive heg.	· Uinc.	end					Initia	1 Leak @ _/	5 "	"Hg = 00	ddo cfm
		6			2					Leak @			
			A Ps	-	Pm	·	Ts			Deak e		Im	COO CIM
	Clock	Dw. Ca-	Direct	Orifi	се ДН	Pump	Stack	Probe	Oven	Effluent	Dry G	as Temp	
Point	Clock	Dry Gas Meter, CF	Pitot in. H ₂ O	in.		Vacuum	Temp		Temp	Temp		F	Remarks
	1	incect, or	111. 1120	Desired	Actual	In. Hg Gauge	° F	°F	°F	°F	Inlet	Outlet	
A-12	17:18	410,308	0.04	3.70	3.20	7.0	290	278	235	56	79	77	
11	20%	413.08	0.04	3.30	3.70	7.0	792	the second second	247	48	80	77	
10	23	415.85	0.04	3,20	320	7.0	294	THE RESERVE THE PROPERTY OF THE PARTY OF THE	248	51	81	1 27	
9	25/2	418,60	0,04	3.20	3.20	20	293	241	251	52	82	77	
8	28	421-60	0,04	370	370	2.0	295		247	53	83	77	
1-3	3042	424.30	0,04	3.70	3.20	7,0	295	THE REAL PROPERTY.	252	53	84		
6	35/2	437,00	0.04	3.20	3.20	7.0	289	257	268	52	86	28	
4	38	4132.90	0.04	320	2.40	5.0	278		255	51	87	78	
3	40/2	435,40	0.02	1.60	1-60	4.0	200	248	261	51	89	78	
2	73	437-50	0.02	1-60	1-60	4-0	280	247	248	52	88		
1	45/2	439.50	0,02	1-60	1-60	4.0	282		255	52	88	79	
END	1244	441.552		-	-			_				-	
13-12	1251	446.552	0.05	4.00	4.00	90	786		271	55	87	29	
1/	531/2	444-60	0.05	4.00	7-00	8.0	289	- Constitution of the last	272	-19	88	79	
10	56	1147.95	0.05	4.00	4.00	810	295	234	273	79	89		
providence of the same of	1301	451.00	0.05	4-06	4.00	8-0	397	234	276	51	90	80	
1201	13011	454.201	0.05	4-00	4-00	851	797	1236	2691	5/	901	80	
Pitot T	ube Cali	bration Fact	or c O	8/8 Pit	ot Tube N	No. 32-	/	Sample	Purge:	Initial		Final	
							- 1		. a. B.	-			0.550
		d Vm 67/7		%CO	2 010	%CO 0 1 C	2	Probe	Tip No.	Initial Pr	robe Tip	Dia. O	498 in
Water C	ollected	Vw 141	2 m1	%0 ₂	21.0	%N2 79	01	V _m = Dry Ga	s Meter	1-9	v	0	498
		6		Are	a Stack A	2 189	in ²	Calibr	ation F	1-9 actor _/- 6	237.6	5.313	-
				Cto	ale			Dry Ga	S	ft ³	-(T.	min x Le	ak etn
Baro. P	ress. Pb	23.30	"Hg	Sta Pre:	ss 0	104 in.	H ₂ O						
								M_{F}	= 3	7-8	M _T =		

PARTICULATE FIELD DATA

Run No.

Location Cooler EX 1

Date 6-31-84

Remarks 322000 Outlet Dry Gas Temp Tm 120000 Inlet 722224 Effluent Temp 26.8 Oven Temp Prole Temp THE 348 297 Stack Temp Vacuum In. Hg Gauge 7.0 7.0 4.0 Pump 2040 4-00 11.00 3.20 2.40 Desired | Actual Orifice AH in. H20 4.00 3.20 1.60 2.40 In. H₂0 0.00 Pitot 5000 40.0 A Ps 473,70 460,40 Meter, CF 463.76 Dry Gas 1303% 58% 13% 187 1831 Clock END # 2000 Point 25

SAMPLE NO.: _	1. Collato	4						
IMPINGER NO.	SOLUTION USED	AMOUNT OF SOLUTION (ml)	IMP. TIP CONFIGURATION	WEIGHT (grams)				
1	DI-H20	100	_ Let 0D	Final 570.1 Initial 576.1 Wt. Gain -6.0				
2	D 7-1-120	100	5. irreely	Final 588.2 Initial 583.9 Wt. Gain 4.3				
3	D14		lung	Final 478.3 Initial 475.6 Wt. Gain 3.7				
4	Silveblus		14:0	Final 815.7 Initial 8/2-5 Wt. Gain 13.0				
5				Final Initial Wt. Gain				
6				Final Initial Wt. Gain				
Flask				Final Initial Wt. Gain				
TOTAL WEI	GHT GAIN OF IMPING	ERS (grams)	14.2					
			DATE: 6-2	1-84				
SIGNATURE: But of the								
ORSAT ANALYSIS RESULTS								
Gas Fractional Part								
CO ₂								
02								
co								
	N ₂							
SIGNATURE:	Mul!	July	DATE: 6-2	1-84				

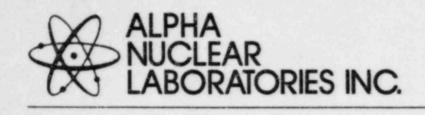
TIME:

APPENDIX E

Analytical Data

PARTICULATION PA	E ANALYSIS	
Date 8-27-84		
Job No. 8410-136		
Name Petrotomics		
Location YCP, fack. Ext., Cooler Eth		
Run No. 1-YED		
Filter No. 1-21 Front Wash 32	5 ml Impinger 1	Impinger 2
Final 0.6738 100.0749		
Initial 0.6380 100.0558		
0.0358 = 35.8 0.0191 = 12.6 33.04	1.5 blank	
MF	mg	
Run No. 1 - Pickaging Exh.		
FilterNo. <u>I-70</u> Front Wash <u>30</u>	00 ml Impinger 1	Impinger 2
Final 0.64/2 112 9758		
Initial 0.6390 112, 9550		
Final 0.64/12 112, 9758 112, 9550 112, 9550 179.5 179.5	20.8 blank	- Livery Com
Final 0.64/12 112,9758 Initial 0.6390 112,9758 $112,9550$ $112,9550$ $112,9550$ $112,9550$ $112,9550$ $112,9550$ $112,9550$ $112,9550$ $112,9550$ $112,9550$	19.5	
MF 21.7 mg MT	mg	
Run No.		
Filter No. 1-69 Front Wash 29	es ml	
	S ml Impinger 1	Impinger 2
Final 0.6516 105.1195		
Initial 0.6443 105.0777 0.0073 = 7.3 0.0318 =	31.8	
Initial 0.6443 105.0777 0.0073 = 7.3 0.0318 = 37.8 mg MT	1. 3 DIONE	
my mi	mg	
Acetone Blank:	D.I.Water Blank	
Final 104 3135		Final
Volume 700 ml Initial 104. 5126	Volumeml	Initial
Blank: 0.0045 mg/ml Total Weight 0.9 mg	Blank:mg/ml T	otal Weight

Blank: ____mg/ml Total Weight _



AND JOSE 64-190

WEST TOWN TOWNER OF THE WYAL

3 000 0007155 FOR RA 226 TH 230 PB 215 U NAT---FOR JOS \$8410-136 PETROTOHIC

SAMPLE I. O.	ISOTOPE	CONCENTRATION (UCI/ML)	LLD(UCI/ML)
RUN I CODLER FRONT 6-21-84	RA-226 TH-230 PB-210 U-NAT	(8.81 ± 4.32) X 10 ⁻¹³ (9.59 ± 3.47) X 10 ⁻¹² (5.76 ± 3.38) X 10 ⁻¹² (6.52 ± 0.02) X 10	6 × 10-13 4 × 10-12 5 × 10-12 2 × 10-13
RUN 1 PACK EXH. FRONT 6-21-84	RA-225 TH-230 PB-210 U-NAT	(1.58 ± 0.74) X (10 ⁻¹² (4.28 ± 33.4) X 10 ⁻¹³ (0.00 ± 7.34) X 10 ⁻¹² (2.65 ± 0.03) X 10 ⁻¹¹	$\begin{array}{cccccccccccccccccccccccccccccccccccc$
RUN 1 YCD FRONT 6-21-84	RA-236 TH-230 PB-210 U-NAT	(5.61 × 2.67) × 10 ⁻¹³ (2.66 ÷ 6.35) × 16 ⁻¹³ (3.07 ÷ 3.21) × 10 ⁻¹³ (6.95 ÷ 0.62) × 10 ⁻¹⁰	3 × 10 ⁻¹³ 9 × 10 ⁻¹³ 5 × 10 ⁻¹³ 3 × 10

CORE LABORATORIES, INC.

P. O. Box 2794 Casper, Wyoming

ANALYTICAL REPORT

er Pertine			**********	************			
				Date	6-26-84	Lab. No. R40	251
ımple				Rn ²²²	Rn222 LLD		
	Van			pCi/l	pCi/T		
	YCD			0.9 ± 0.3	0.2		
	Packaging Cooler ex	haust		$\frac{0.1 \pm 0.3}{0.1 \pm 0.3}$	0.2		_
		-		-			_
							Name of Street
	-						-
	-	-					-
		-					
-							
				-			-
						-	-
				-			
	THE STATE						-
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APPENDIX F

Chain of Custody and Analysis Request

WESTERN ENVIRONMENTAL SERVICES & TESTING

Chain of Custody and Analysis Request

Job Numbe	841	0-136	Date((s) Sampled	6-21-8	84
Job Name	Potro	Townes		er of Runs	3	
		cley Bother,	wy.			
Unit Test	ed /CD-	cooler -	HACK- C	d.		
		Absorbing Solu	rtion/Analysi	.s ror		
Run	Filter Number	Imp 1	Imp 2	Imp 3	Imp 4	Probe Wash
1-40	I-71	VI 1120	021/20/	DRY	5111c+ 649/	Acethe
1-1 mg = X4	エーショ	4	*	,	,	",
1 - Cooler	I-7/ I-70 I-69	4	7	v	4	и
4		THE STATE OF THE S				
No _x :						
Other						
Total Num	ber of Sample	Bottles:	3			
Total Num	ber of Filter	rs:3	,			
Comments:						
-			11 /	11/1		
Person Res	sponsible for	Samples:	13.1.	lely		
Sample No.	Recovered	i by	Date	Time	Location	
1	Buch	1.1/10	6-21-8	4 10:15	On 9,7	3
2	1/201	17/16	1 6-21-8			
3	Burg	1. There	1 671-1			
4		V				
Samples Ro	eceived by	13 11/2	of for y	ansport Dat	e:6-21-84 Ti	me: 1400
Samples Re	eceived at la	ib by 15	111/1		e:62-5-71in	
Samples Ar	nalyzed by	alan He	mance		e: 8-1/-84Ti	
		1				

APPENDIX G

Resumes of Test Personnel

BRUCE A. HINCHEY

CURRENT: 6-1-81 to present President, Western Environmental Services and Testing, Inc., Casper, Wyoming, Dallas, Texas, and Bismarck, North Dakota; an environmental monitoring and consulting firm.

PROFESSIONAL: 6-1-78 to 5-31-81

Vice President, Air Quality Department, Kumpe and Associates, P.C., Casper, Wyoming; an engineering and consulting firm.

9-1-72 to 6-1-78

Manager, Air Quality Studies, Ecology Audits, Inc., an environmental monitoring and consulting firm. Former Laboratory Manager for same in Casper, W, oming.

EDUCATION:

Attended the University of Missouri at Rolla for $3\frac{1}{2}$ years; Major - Petroleum Engineering.

TECHNICAL EXPERIENCE:

Managed over 120 ambient air studies in the past years; managed the operation of 40 ambient air networks at Wyoming coal and uranium mines; conducted over 1500 source emission surveys in the western and southwestern United States; qualified as an expert witness in air pollution litigation.

TEACHING EXPERIENCE:

Lectured in the U. S. Environmental Protection Agency's training course "Source Sampling for Particulate Pollutants," September 1975; lectured in short course "Performing and Observing Source Sampling," May 1977; conducted source sampling training for industrial personnel at various locations.

PROFESSIONAL TRAINING:

Attended short course for consultants "Performing and Observing Source Sampling," Dallas, Texas, 1976; E.P.A. short course, "Source Sampling Techniques and Reporting," Denver, Colorado, December 1976; National Asphalt Producers Association short course, "Asphalt Plant Construction, Design and Servicing for Air Quality," December 1977.

CERTIFICATIONS:

Visible Emissions Evaluator Licensed Private Pilot, multi-engine-land, instrument rated

PROFESSIONAL MEMBERSHIPS:

Air Pollution Control Association
Society of Petroleum Engineers of A.I.M.E.
Society of Mining Engineers of A.I.M.E.
Source Evaluation Society
Wyoming Mining Association
Colorado Mining Association

MARCELO A. VINCENT

CURRENT: October 1983 to present

Technician, Western Environmental Services and Testing, Inc., Casper, Wyoming and Bismarck, North Dakota; an environmental monitoring and consulting firm.

PROFESSIONAL: 3/15/83 to 7/15/83

Loss Prevention Agent, Internal Loss Investigations, J.W. Robinson Company, Pasadena, California

7/80 to 10/82

Security Officer, Casper College, Casper, Wyoming

5/75 to 4/79

Law Enforcement Specialist, United States Air Force

EDUCATION:

Attended Los Angeles City College, Los Angeles, California and Casper College, Casper, Wyoming, for 1½ years. Currently attending Casper College majoring in Criminal Justice.