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# RELAP5/MOD3 Code Manual

User's Guidelines

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Prepared by  
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Prepared for  
U.S. Nuclear Regulatory Commission

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# RELAP/MOD3 Code Manual

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## ABSTRACT

The RELAP5 code has been developed for best-estimate transient simulation of light water reactor coolant systems during a severe accident. The code models the coupled behavior of the reactor coolant system and the core during a severe accident transient, as well as large and small break loss-of-coolant accidents and operational transients, such as anticipated transients without scram, loss of offsite power, loss of feedwater, and loss of flow. A generic modeling approach is used that permits as much of a particular system to be modeled as necessary. Control system and secondary system components are included to permit modeling of plant controls, turbines, condensers, and secondary feedwater conditioning systems.

RELAP5/MOD3 code documentation is divided into five volumes: Volume 1 describes modeling theory and associated numerical schemes, Volume 2 contains detailed instructions for code application and input data preparation, Volume 3 provides the results of developmental assessment cases that demonstrate and verify the models used in the code, and Volume 4 presents a detailed discussion of RELAP5 models and correlations. Volumes 1-4 are in varying stages of development. This document, Volume 5, contains guidelines that have evolved over the past several years through use of the RELAP5 code.

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The decision concerning whether this document should include all the work done by past users has been difficult. Inevitably some people's work has not been included. In general, the authors have decided whether to include a particular piece of work based on its application to RELAP5/MOD3. Most past work has been done using earlier versions of RELAP5.

The authors are particularly grateful to Gene S. Rhee, David Bessette, and Louis M. Shotkin of the U. S. Nuclear Regulatory Commission for their support and suggestions over the past months. In addition, the authors are indebted to Vic Ransom and his students at Purdue University for their review and critique. Finally, the authors are also very grateful to Nancy Larson and Edna Johnson as the RELAP5 Newsletter editors, to Clay Miller and Rich Triemke for their development support, to James Cozzuol and Chris Allison for their reviews, and to Mary Harris, Erma Jenkins and Evelyn Onkes for their work on the illustrations and appendices.



# RELAP5/MOD3 CODE MANUAL

## VOLUME 5: USER'S GUIDELINES

### EXECUTIVE SUMMARY

The RELAP5/MOD3 advanced-thermal hydraulic code has become a tool used throughout the world to analyze transients in light water reactor systems. RELAP5/MOD3 code users range from world-renowned thermal-hydraulic experts to college students. Thus there is a great need for guidelines to use the code.

The RELAP5/MOD3 user's guidelines manual is a loose-leafed document and will be updated periodically. There are two reasons for this:

- The MOD3 version of the code has only been available to the world community for about a year so there has not been enough time for many MOD3-specific guidelines to be produced. Most of the user's guidelines are based on work done using RELAP5/MOD2.
- In a sense, user's guidelines are never complete. As more and more experience is gained using the code, additional guidelines will be defined and included.

The user's guidelines have been designed for both first-time users and experienced users. As such, the entire analysis process is outlined and described. Essentially, the model construction process consists of the following steps:

- The transient scenario should first be evaluated from the perspective of whether the code has the capability to analyze the expected phenomena. For example, if three-dimensional neutronics effects are important, the analyst should realize RELAP5/MOD3 does not have the capability to analyze such transients. However, the code can be used to analyze many other important transients.
- The information required to build the model must be collected. This information consists of system geometry specifications and system initial and boundary conditions.
- The information that describes the hardware as well as the hardware initial and boundary conditions must be "translated" to the form required by RELAP5/MOD3.
- The nodalization resulting from the above process should be reviewed by a model review committee before performing an analysis. The committee will review the important phenomena that will occur during the transient and determine whether the model and planned analysis approach will be adequate to evaluate the transient behavior and meet the analysis objectives.
- The steady-state calculation is performed and analyzed. The analyst must ensure

that the model initial condition is representative of the real system's condition.

- The transient calculation is performed and analyzed. During this phase of the analysis process, the analyst must ensure that the code results are representative of the subject transient. Unphysical results caused by improper nodalization, code deficiencies, or user errors must be identified and eliminated. Thereafter, the analyst can use the results to meet the desired analysis objectives.
- Throughout the process, the analysis must be rigorously documented. The model should be documented in a workbook and independently checked, when feasible, by another analyst. The calculation should be outlined, the steps taken to ensure that the calculation is representative of the subject transient should be listed, and the analysis results should be recorded.

The above seven-step process should be used whether performing a code assessment calculation or a code application calculation [i.e., whether assessing the code by comparing the calculation to a data set or applying the code to predict the behavior of a thermal-hydraulic system (a commercial power plant) for example]. Most of the above steps are illustrated with a typical Westinghouse plant model. Questions concerning application of the code to Combustion Engineering, Inc. and Babcock & Wilcox plants are answered in subsections specific to these plant types.

## 1. INTRODUCTION

The RELAP5/MOD3 code is the third major variant of the RELAP5 advanced thermal-hydraulic code that was released in 1979 (Ransom et al., 1979). Initially, this code was used principally by Idaho National Engineering Laboratory (INEL) analysts for understanding Loss-of-Fluid Test (LOFT) and Semiscale experimental behavior. Since then, the code has become widely accepted throughout the world for analyzing commercial and experimental light water reactor systems together with their related associated systems.

Through evolution and use, the code has become more complex while the user base has appreciably increased. The number of problem types the code can handle has also increased. Consequently, the code has become more difficult to use and there is a broader range of analyst abilities. That is, some analysts are novice users with only elementary training in thermal-hydraulic phenomena, whereas other users are world-class thermal-hydraulic experts.

Because of the code's versatility and widespread use, the novice user may be tempted to assume that the code can be used with impunity to study any light water reactor transient. This is not the case. The user's guidelines given in the following pages outline restrictions and cautions that users should exercise when performing thermal hydraulic analyses.

This document has been designed to guide all classes of RELAP5/MOD3 users to produce quality models and analyses concerning the thermal-hydraulic behavior of light water systems that are consistent with the current knowledge concerning the code. Volume 5 is unlike the other volumes in that it is a "living document" that will be updated when (a) information is provided by the user community from code assessments and applications studies, (b) corrections are generated, and (c) user's guidelines for SCDAP and ATHENA are assembled.

This volume has been organized to provide user guidelines in the order of increasing detail. Section 2 gives modeling techniques from an overall perspective and a very general outline of whether to use the code for a specific application. Section 3 gives advice concerning overall model construction including general code model options, and Section 4 gives specific guidelines applicable to each component model available in the code. As a result, the more advanced users will probably discover that their questions are addressed in the later sections of the report. Finally, Section 5 consists of examples showing how the code has been applied to analyzing pressurized water reactors (PWRs).

## 2. FUNDAMENTAL PRACTICES

Problems concerning the behavior of single- and two-phase fluid systems are often too complex and/or unwieldy to use hand calculations. Consequently, a number of advanced thermal-hydraulic codes have been created (e.g., RELAP5/MOD3, TRAC-PF1/MOD2, etc.), and are a part of the analyst's tool-chest. Once the potential code user is aware of the existence of such tools, the decision to use a particular code should hinge on the answers to the following questions:

- Does the code have the capability to handle the problem?
- What kind of equipment is needed to use the code? If the user must analyze the problem on a mainframe computer, is use of the code affordable?
- If the code does have the capability to analyze the problem and the necessary computing hardware is available, what is the best way to apply the code?

The purpose of Section 2 is to discuss the first and third bullets above. Hardware requirements are discussed in Volume 2.

### 2.1 Capability of RELAP5/MOD3

RELAP5/MOD3 analyzes the thermal-hydraulic behavior of light water systems. It was originally designed to analyze complex thermal-hydraulic interactions that occur during either postulated large or small break loss-of-coolant accidents (LOCAs) in PWRs. However, as development continued, the code was expanded to include many of the transient scenarios that might occur in the thermal-hydraulic systems. Thus, the code has been successfully used to analyze not only large (Brittain and Aksan, 1990) and small (Fletcher and Kullberg, 1985; Fletcher et al., 1985) break LOCAs, but also operational transients in PWRs (Stubbe, 1986; Schultz et al., 1984; Chung, 1990) and various transients in experimental and production reactors and reactor simulators (Rosdahl and Caraher, 1986; Croxford and Hall, 1989; Megahed, 1987). The code has also been used (to a lesser extent) for boiling water reactor (BWR) system analysis (Dallman et al., 1987; Schultz and Wagoner, 1982; Eriksson, 1989).

The RELAP5/MOD3 equation set gives a two-fluid system simulation using a nonequilibrium, nonhomogeneous, six-equation representation. The presence of boron and non-condensable gases is also simulated using separate equations for each. Constitutive models represent the interphase drag, the various flow regimes in vertical and horizontal flow, wall friction, and interphase mass transfer. The code has a point kinetics model to simulate neutronics. The field equations are coupled to the point kinetics model, thus permitting simulation of the feedback between the thermal-hydraulics and the neutronics. The code also has the capability to simulate the presence of slabs of material adjacent to the fluid. Thus, energy transfer to and from stationary slabs of material can be simulated. Control systems and component models permit simulations of equipment controllers, balance-of-plant equipment (e.g., turbines, pumps, and condensers), and lumped-node representations of various processes (e.g., heat transfer from one volume to another).



The RELAP5/MOD3 code has implied capabilities because (a) the equation sets formulated for the RELAP5/MOD3 code were designed to investigate light water system behavior at both nonhomogeneous and nonequilibrium conditions and virtually any pressure between the critical and atmospheric states, (b) the point kinetics model allows the study of various anticipated transients without scram (ATWS) and the thermal-hydraulic and neutronics feedback effects, and (c) the code's control systems capabilities and balance-of-plant models allow a coarse simulation of virtually any component of a plant using a "lumped node" approach. The user may be tempted to assume that the code can be used with impunity to study any light water reactor transient. This is not the case, however. The restrictions and cautions that the user must exercise when confronted with a problem that requires analysis are discussed below.

### 2.1.1 Assessing Use of the Code

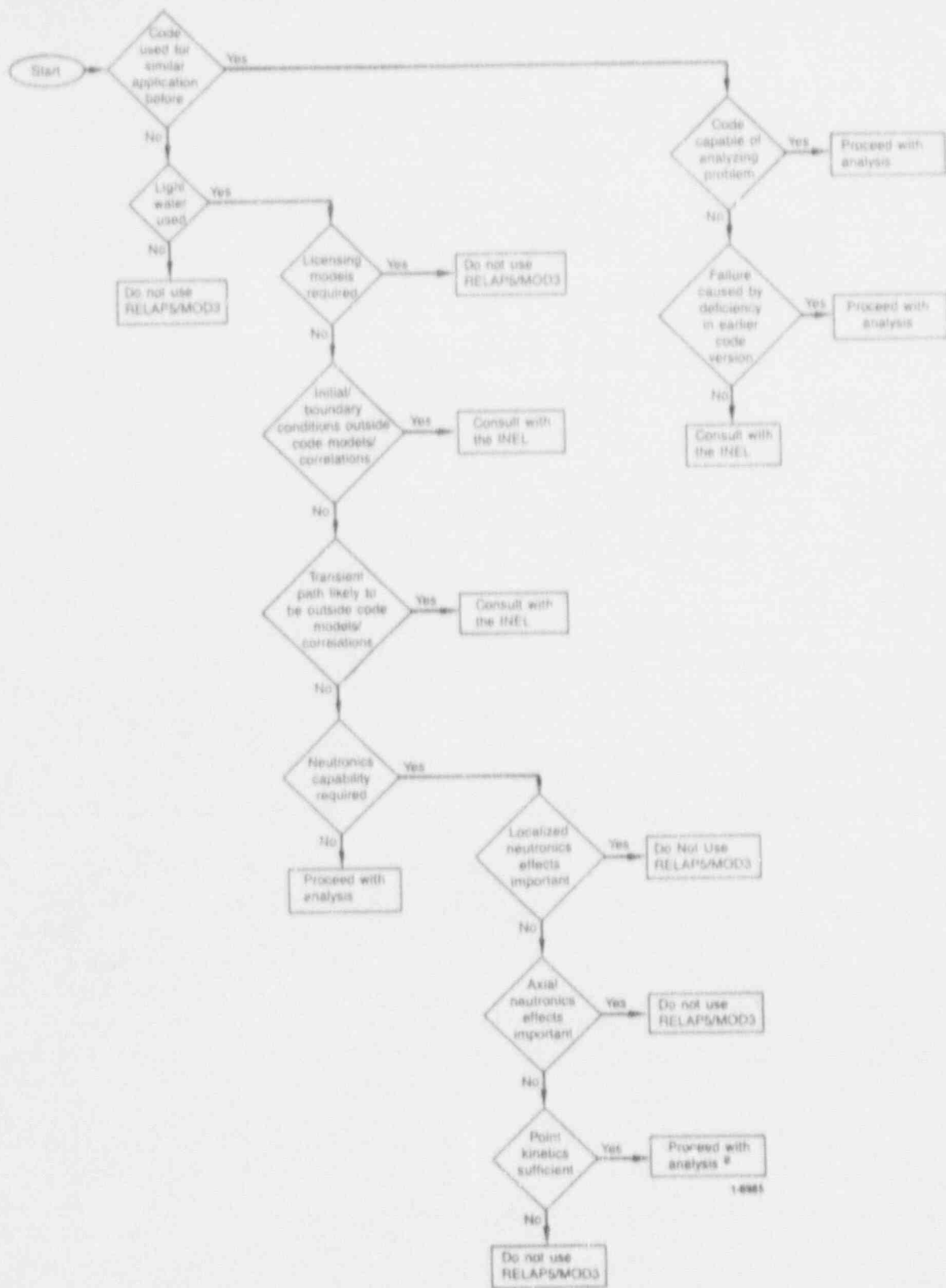
RELAP5/MOD3 has been used by analysts to evaluate the thermal-hydraulic behavior of many light water systems. Consequently, several reference documents exist for the potential user (see Appendix A for abstracts of these documents). This body of literature can aid in determining whether a problem can be evaluated by the code. If the user is faced with a unique application or a problem that previously was determined to be beyond the capability of the code, the logic path outlined in Figure 2-1 should be used as a guide.

A subset of problems that falls within the analysis in Figure 2-1 deserves special mention. RELAP5/MOD3 and earlier versions of the code have been used for structural analysis (including water and steam hammer) in the past. Since such problems must be treated with great care, the next subsection is devoted to them alone.

### 2.1.2 Structural Analysis Using RELAP5

The RELAP5 code was developed principally to calculate fluid behavioral characteristics during operational and LOCA transients. Of course, the results describing fluid behavioral characteristics provide the basis for also calculating structural loading because the transient hydrodynamic pressures are key results. Furthermore, RELAP5 will calculate acoustic wave propagation (pressure signal transmission) in pipelines and various system components. However, it is important to understand and carefully evaluate RELAP5 results that are used in such a way.

First, the potential user should know that structural loading analysis was not part of the charter that led to creation of the code. Therefore, the RELAP5 numerical techniques were not optimized for such an application. Second, rigorous assessment of the code's results concerning structural loading has never been undertaken. Consequently, there are no official benchmark calculations that verify the code's capability for performing such calculations or give a suggested approach that is known to work. Third, the RELAP5 solution scheme is designed to converge based on a mass continuity equation-based Courant limit (i.e., the numerical algorithms reduce the solution time step based on the mass flow transit time through each component cell). Because of this, pressure wave propagation will violate the Courant limit unless special care is observed by the user. The following two sections offer advice concerning structural analysis and acoustic wave propagation (water or steam hammer).



a. If the user intends to conduct a structural, water hammer, or steam analysis using RELAP5/MOD3, consult section 2.1.2.1 or 2.1.2.2.

Figure 2-1. RELAP5/MOD3 use analysis.

**2.1.2.1 Structural Analysis.** A program has been written that computes fluid induced forces using the RELAP5/MOD3 hydrodynamic output. The code is called R5FORCE/MOD3s (Watkins, 1990) and is based on a one-dimensional representation of the momentum equation that

- Neglects fluid velocity and shear force effects that are external to the flow path
- Assumes a one-dimensional uniform cross-sectional area control volume
- Approximates the normal stress by the quasi-steady change in the momentum
- Represents uniformly the fluid velocity, density, and pressure over the local cross-sectional area and the shear over the local control volume surface area.

However, as Watkins has stated in the R5FORCE/MOD3s manual: "It must be understood that verification studies with R5FORCE/MOD3s program have been very limited and no comparison with experimental data have yet been made" (Watkins, 1990).

**2.1.2.2 Water and Steam Hammer Analysis.** Using the code for water and steam hammer analyses is sometimes a controversial topic. Analyst's opinions range from not using the code to using the code with qualifications. At the heart of the various differences in opinion are the finite differencing scheme used in the code and the standard practices exercised by most users. The code differencing scheme is the upwind or donor-cell scheme. The standard practices exercised by most users are based on their experience with the code in solving thermal-hydraulic phenomenological problems related to defining system mass distribution, core heatup, etc.

Fundamentally, researchers investigating the behavior of the upwind or donor-cell differencing schemes have shown that for the nodalization schemes used by most thermal-hydraulic analysts in RELAP5 type problems, an acoustic wave is rapidly attenuated (Stuhmiller and Ferguson, 1979; Oran and Boris, 1987). Thus, if a user attempts to use the code for water or steam hammer analysis, very close attention must be paid to the cell size and time step. Two factors must be considered very carefully for such analyses: (a) the Courant limit with regard to the acoustic wave must be manually tracked and (b) the cell size should be decreased so that there are a number of cells over the region of the pressure wave that has a high rate of change.

The acoustic wave Courant limit is the time required for a wave traveling at the sonic velocity to pass through any given model cell. Since the sonic velocity can be quite high, the time step usually has to be reduced to a rather small number. Also, if the pressure wave is expected to have a very rapid rate of increase, then the cell nodalization scheme must be implemented to give a small length dimension. Working with these restrictions, the ratio of the model cell length to the solution time step (i.e.,  $\Delta x/\Delta t$ ) will be a large number for most water or steam hammer applications. An informal study done by Watkins<sup>a</sup> in 1982 using RELAP5/MOD1 showed that  $\Delta x/\Delta t$  ratios of 6100 m/s gave reasonable results for a 0.34-m diameter pipe filled with 75 K

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a. Private communication with John C. Watkins, EG&G Idaho, Inc. Idaho Falls, Idaho, January 1991.

subcooled water at 15.5 MPa. However, at  $dx/dt$  ratios of 61,000 m/s the solution exhibited "ringing," and at  $dx/dt$  ratios less than 610 m/s the wave was rapidly attenuated and distorted. When confronted with the need to do a water hammer analysis on the Braidwood Unit 1 Nuclear Power Plant residual heat removal piping, another user concluded that the long pipe lengths combined with a sonic velocity of approximately 1500 m/s created a problem that the RELAP5 code was not well-suited to handle.<sup>b</sup> Therefore, people planning to use RELAP5 for water or steam hammer analyses are cautioned to carefully examine the application and compare the code's prediction to their expected result. If the user has any doubts concerning the ability of the code to give an undistorted result, then a code designed specifically for acoustic wave propagation analysis is recommended.

## 2.2 Description of Thermal-Hydraulic Analysis

Once the analyst has decided to use RELAP5/MOD3 to analyze a problem, obtaining the problem solution consists of the following stages:

- Gathering and organizing information that defines the initial and boundary conditions. All the available information must be divided into two categories: pertinent and nonpertinent. Missing information must then be obtained from sources such as vendors, utilities, or consultants to provide the complete spectrum of needs for the code. A problem description and solution notebook is started to document the problem solution and chronology of the work.
- Defining and nodalizing the problem. The code input nodalization should be defined so the most complete information set concerning the questions that motivated the study will be available. The solution approach, assumptions, and final model nodalization are recorded in the model workbook. This stage also includes the formation of a design review committee to conduct reviews of the model nodalization and the analysis approach.
- Inputting the problem. The initial and boundary conditions are placed in a computer file. The model is then initialized to secure the desired starting point for the problem investigation and the proper boundary conditions. The experience is recorded in the problem description and solution notebook.
- Running the code and analyzing the problem. The code is run until completed, and the solution is analyzed. All analysis procedures, findings, and observations are recorded in the problem description and solution notebook.

Each of the four phases described above is described in more detail in the following four sections.

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b. Private communication with Victor T. Berta, EG&G Idaho, Inc., Idaho Falls, Idaho, January 1991.

## 2.2.1 Gathering and Organizing information

Fundamentally, the RELAP5/MOD3 input requirements can be divided into four distinct areas: hydrodynamics, heat structures, control systems, and neutronics. The overall inputs required are listed below:

- Hydrodynamics
  - All flow areas
  - All flow lengths
  - Vertical orientations
  - Geometric detail sufficient to calculate hydraulic diameters
  - Material roughness at fluid-wall interfaces
  - Information sufficient to calculate flow losses (e.g., bend geometries, area expansion geometry, valve geometries, rated or test valve flow rates, plant startup test data)
  - Initial plant conditions
  - Pump characteristics
- Heat structures
  - Material thicknesses
  - Material masses
  - Pipe lengths
  - Inner and outer diameters
  - Material types
  - Material properties as a function of temperatures (e.g., thermal conductivity, density, and specific heats)
  - Heater power (if the mass has source terms)
  - Locations of heat sources
  - Initial temperature distributions



- Control systems
  - Control system block diagrams
  - Identification of the relationship between various control systems and the hydrodynamic and/or heat structures that are controlled
  - Controller characteristics
    - Filter characteristics
    - Setpoints
    - Gains
    - Saturation limits
    - Lags
  - Controlled equipment characteristics
    - Valve stroke rates
    - Maximum/minimum pump speeds
    - Maximum/minimum cycling rates
  
- Neutronics
  - Initial reactivity
  - Exposure data
  - Delayed neutron fraction data
  - Fission product yield fraction
  - Actinide yield fractions
  - Reactivity characteristics.

This information is available in various system specific documents. The following items are examples:

- Final safety analysis reports
- Prints of loop piping
  - Reactor set
  - Steam generator
  - Steam lines

- Feed train
- Pressurizer
- Reactor coolant pumps
- Accumulators
- Safety injection lines
- Piping and instrumentation diagrams
- Precautions, limitations, and specifications documents
- Operating procedures
- Fuel and reactor kinetics information
- Pump characteristics
  - Reactor coolant pumps
  - Emergency core cooling pumps
  - Charging pumps
  - Main feedwater pumps
  - Auxiliary feedwater pumps
- Valve information
- Plant startup test data.

Each of the information sources should be listed in the problem description and solution notebook. As information is taken from each source and used to calculate RELAP5-specific input, the information source can be specified in each instance.

### 2.2.2 Defining and Nodalizing the Problem

Following receipt of all the pertinent information regarding the system to be modeled, the next step consists of isolating the important components of the system that must be modeled using the code. In effect, the user must draw a boundary around the system that requires simulation. The boundary defines the extent of the model and the model is composed of volumes that are called "control volumes." The "control volumes" are defined by the user in a fashion that best allows analysis of the problem. The process of creating the "control volume" is called "nodalizing the model." During the process of defining and nodalizing the problem, *the user must*

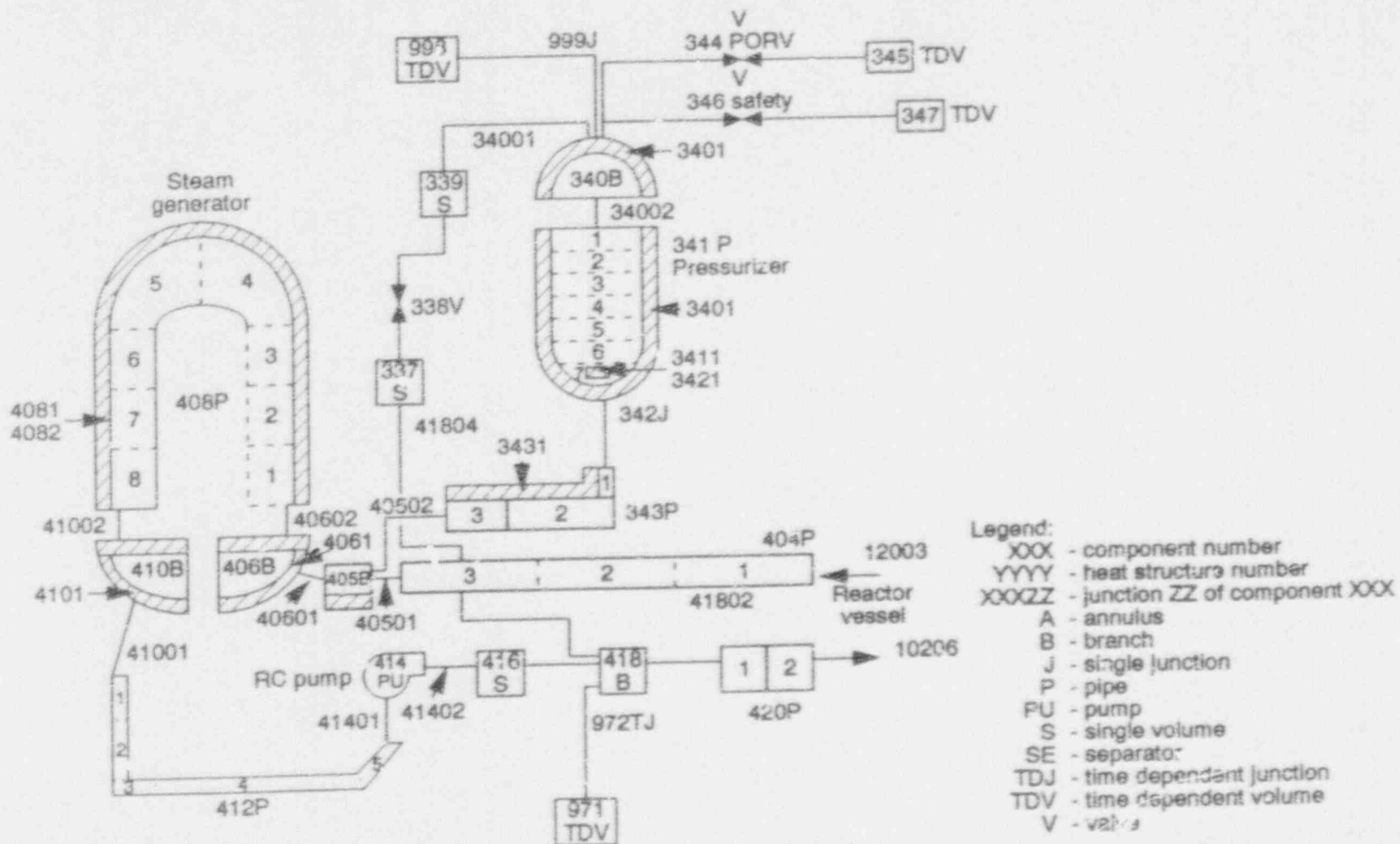
carefully document each step. When the documentation process is completed, the model should be checked by an independent checker.

**2.2.2.1 Definition of the Model Boundary.** Usually, definition of the model boundary is straightforward. The exact location of the model boundary is dependent on the type of problem being analyzed. That is, if the user is only interested in core heatup characteristics for a particular PWR and the core inlet and outlet conditions (together with the core power) are known as a function of time, then the model boundary could be placed to only include the core together with the core inlet and exit flow paths. On the other hand, if the entire primary system behavior for the same PWR requires study, then the model boundary would probably encompass the entire primary system, together with the portion of the secondary system that interfaces with the primary. The extent to which the secondary system is simulated depends on the problem. For example, if the user is analyzing an LOCA that results in closure of the secondary system's main steam line valves early in the transient, then only that portion of the secondary system from the steam generators up to and including the main steam line valves need to be modeled. On the other hand, if the user is analyzing a plant event that involves interactions between the various components of the balance-of-plant equipment (i.e., the turbines, the condensers, feed pumps, booster pumps, etc.) then the crucial balance-of-plant equipment components would also have to be included in the model boundary.

An example of a one-loop PWR model, with the model boundaries defined to include the entire primary system and the secondary system up to the turbine stop valve (the turbine is crudely simulated using a boundary condition), is shown in Figures 2-2, 2-3, and 2-4. Such a model was designed to analyze plant operational transients that did not include pipe breaks and for which balance-of-plant components exerted little or no influence on the course of the transient.

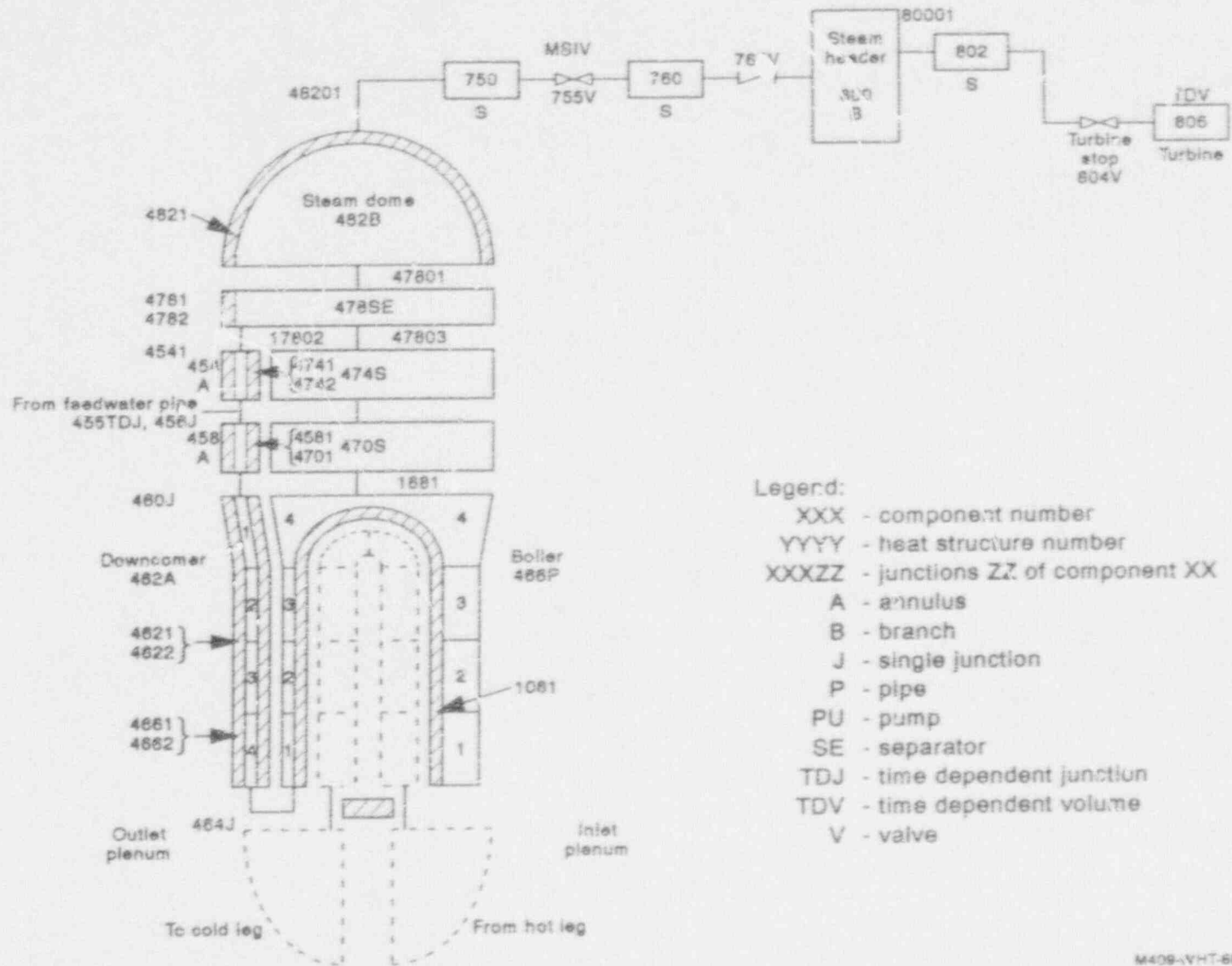
**2.2.2.2 Model Nodalization.** Following definition of the model boundary, the next step is to nodalize the model. That is, each portion of the model must be divided into discrete components. As stated in Volume 2: "RELAP5 is designed for use in analyzing system component interactions as opposed to detailed simulations of fluid flow within components. As such, it contains limited ability to model multidimensional effects either for fluid flow, heat transfer, or reactor kinetics" (Carlson et al., 1990a). Consequently, the model is divided into control volumes that are essentially stream tubes having inlet and outlet junctions. The junctions connect the various model control volumes together. The code calculates the average fluid properties at the center of the control volumes throughout the model and the fluid vector properties at the junctions.

The simplest subdivision of a model into a set of control volumes or nodes is obtained by dividing the entire model into approximately equally-sized nodes. Fundamentally, the maximum node size is determined by the Courant limit (i.e., the node length divided by the maximum fluid velocity determines the limiting maximum time step size). However, an additional factor influencing the node size, based on the accuracy and limitations of the averaged one-dimensional



M409-WHT-891-03

Figure 2-2. Nodalization of primary loop.

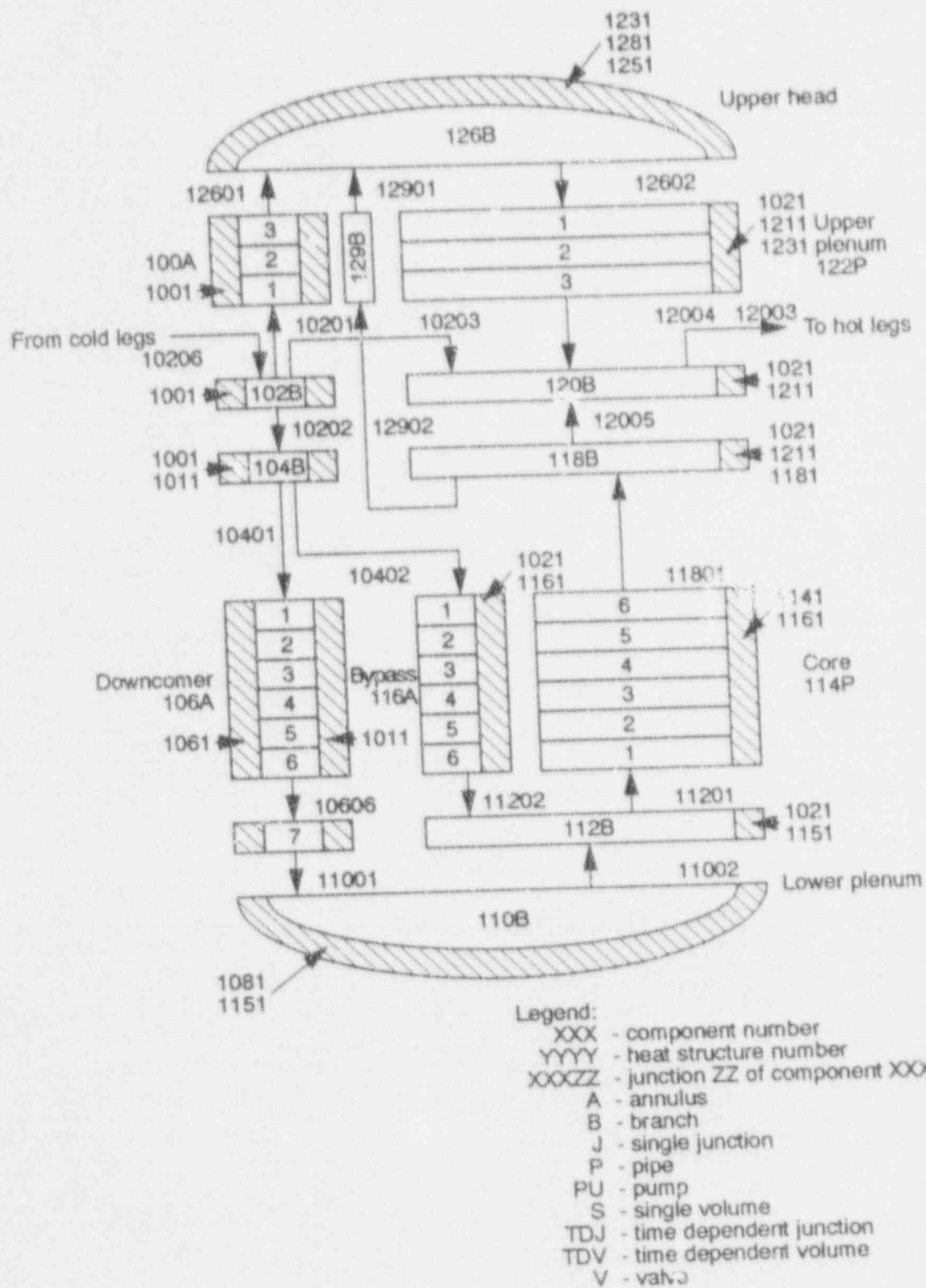


- Legend:
- XXX - component number
  - YYYY - heat structure number
  - XXXZZ - junctions ZZ of component XX
  - A - annulus
  - B - branch
  - J - single junction
  - P - pipe
  - PU - pump
  - SE - separator
  - TDJ - time dependent junction
  - TDV - time dependent volume
  - V - valve

M409-VHT-661-01

Figure 2-3. Nodalization of steam generator and secondary system.





M409-WHT-891-02

Figure 2-4. Nodalization of reactor vessel.

formulation numerical stability, is the ratio of the node length to the node hydraulic diameter. The length-to-diameter ratio should be greater than or equal to one. Considering both criteria, a typical model control volume length can be specified for the problem to run efficiently.

However, it should be recognized immediately by the user that unless the model is quite simple, the model cannot be subdivided into equally-sized nodes. Practical hardware configurations are often complex and may contain multiple flow paths that change both area and orientation in the direction of fluid flow.<sup>c</sup> Also, in some portions of a system, single-phase fluid may move in a quiescent fashion while in other portions of the system the fluid may be highly agitated and exist in both the liquid and gaseous phases. The user will usually be more interested in the fluid behavior in one portion of the system boundary than in another. Consequently, finer nodalization may be used to study the fluid behavior in specific locations of the model.

The model shown in Figures 2-2, 2-3, and 2-4 has been subdivided into a number of nodes. For example, the pressurizer was divided into eight nodes (Figure 2-2). Seven of the nodes are contained within a RELAP5 PIPE component (component 341) and one node is simulated using a RELAP5 BRANCH component (component 340).<sup>d</sup> It should be noted that the calculations required to specify the dimensions, properties, and fluid conditions within each node must be documented and kept within the problem description and solution notebook. An example of such a calculation for a portion of the pressurizer is shown in Figure 2-5.

Modeling most systems requires not only simulating the fluid stream tubes but also stationary mass (heat slabs) that have the capability to store heat or might even contain heat sources. The code has the capability to simulate one-dimensional heat transfer from heat slabs to the fluid. Generally, the heat slabs are nodalized to have a length-dimension that is no longer than their adjacent fluid control volumes. Sometimes, depending on the specific application, the heat slabs have length-dimensions that are less than their adjacent control volume. Examples of heat slabs are shown in Figures 2-2, 2-3, and 2-4. Thus, the heat slab modeling the pressurizer dome material adjacent to control volume 340 is number 3401 in Figure 2-2. The heat slabs simulating the core barrel and the exterior wall of the reactor vessel in the downcomer region (control volume 106 in Figure 2-4) are 1011 and 1061, respectively.

As the analyst plans and constructs the model, a design review committee should be formed. The purpose of the committee is to not only review the planned analysis approach, but also to suggest model improvements and additional areas of investigation. The committee should be composed of individuals that are experienced in the area of investigation. Of special importance is the model nodalization. The model should be nodalized based on the results of past nodalization studies and on the particular requirements of the analysis.

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c. The user should make every effort to minimize the flow paths that are included in the model. As an example, tiny flow paths that may physically be present to cool hardware but are inconsequential to the overall system behavior should not be included. Inclusion of such flow paths will slow the problem run time and often give inaccurate results.

d. The RELAP5 components are discussed in detail in Section 4.

CALCULATION WORK SHEET

Page 1 of        Pages  
 Subject PRESSURIZER NODALIZATION Date 4/83  
 Prepared By J. Z. Steiner Checked K. K. Brown Work Request       

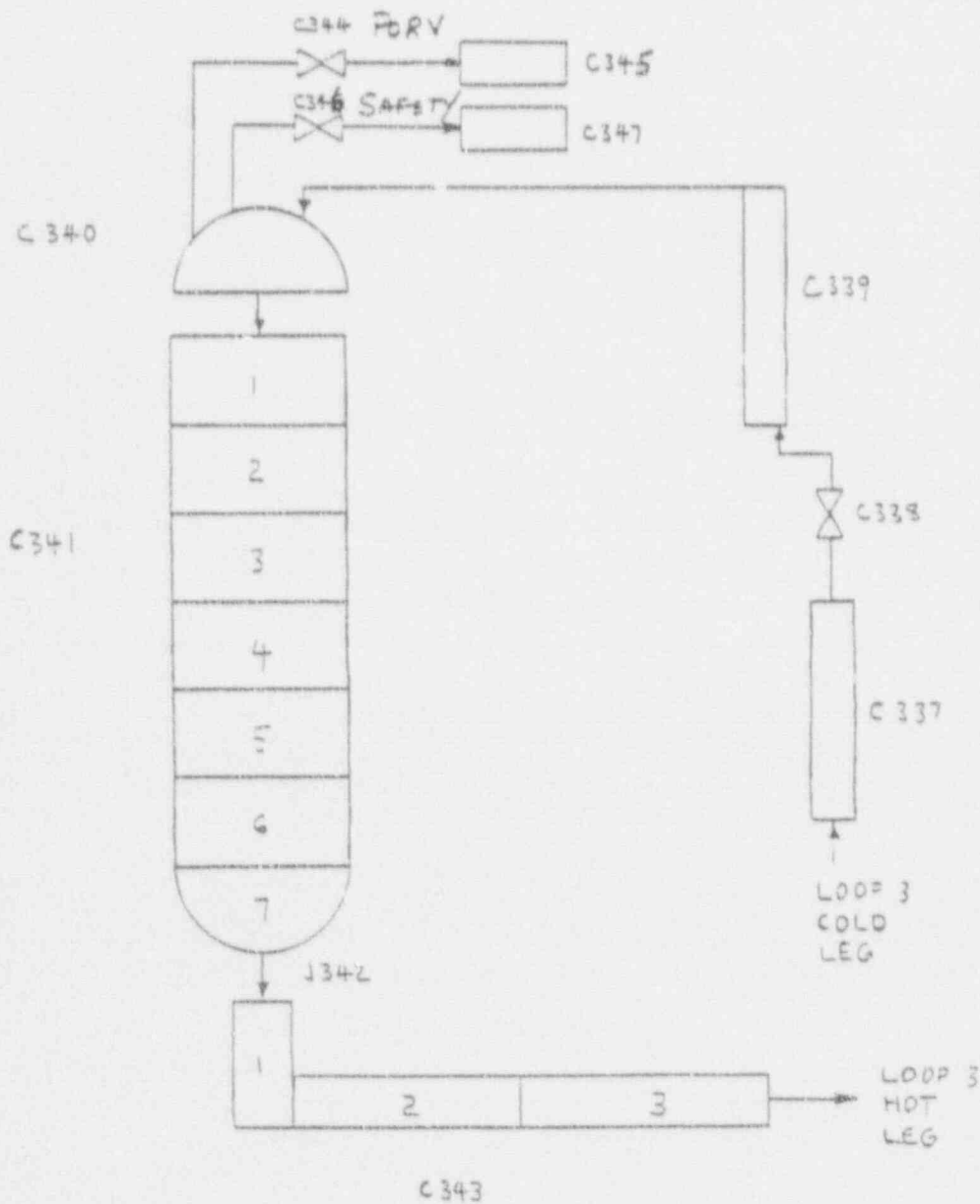


Figure 2-5. Calculation worksheet for pressurizer nodalization.

CALCULATION WORK SHEET

Page 2 of \_\_\_\_\_ Pages

Subject C 340

Date 4/83

Prepared By J. Z. Steiner Checked E. C. Logsdon Work Request \_\_\_\_\_

COMPONENT 340 (BRANCH)

REGION REPRESENTED:

HEMISPHERICAL UPPER HEAD OF PRESSURIZER

JUNCTIONS:

- 34001 PRESSURIZER SPRAY LINE
- 34002 CONNECTION TO LOWER PART OF PRESSURIZER

INNER RADIUS = 42" (P S. 4.6-2 FSAR)

$$V_{340} = \frac{1}{2} \left\{ \frac{4}{3} \pi \left( \frac{42}{12} \text{ ft} \right)^3 \right\} = 69.7972 \text{ ft}^3$$

$$L_{340} = 42" = 3.5 \text{ ft}$$

$$\begin{aligned} \text{JUN AREA}_{34001}^C &= \text{AREA OF 4 in. SCH 160 PIPE (P 44 S.D. - 1)} \\ &= .0645 \text{ ft}^2 \quad (\text{P 3-17 CRANE}) \end{aligned}$$

$$\text{JUN AREA}_{34002} = \pi \left( \frac{42}{12} \text{ ft} \right)^2 = 38.4845 \text{ ft}^2$$

Figure 2-5. (continued).

**CALCULATION WORK SHEET**

Subject C 340 Page 3 of        Pages  
 Date 4/83  
 Prepared By J. L. Steiner Checked K. C. Upson Work Request       

**SPRAY NOZZLE LOSS COEFFICIENT :**

SPRAY NOZZLE  $\Delta P = 15$  PSI AT 600 gpm AND 70°F (S.D.-1)

$$K_{34001} = \frac{2(A_{34001})^2 \Delta P \rho}{m^2}$$

AT 70°F, 2250 PSIA:  $\rho = 62.74 \frac{\text{lbm}}{\text{ft}^3}$

$A_{34001} = .0645 \text{ ft}^2$  (P 2)

$$K_{34001} = \frac{2(.0645 \text{ ft}^2)^2 \cdot 15 \frac{\text{lb}_f}{\text{in}^2} \cdot 62.74 \frac{\text{lbm}}{\text{ft}^3}}{\left(600 \frac{\text{gal}}{\text{min}} \cdot 62.74 \frac{\text{lbm}}{\text{ft}^3} \cdot \frac{.134 \text{ ft}^3 \text{ min}}{\text{gal} \cdot 60 \text{ sec}}\right)^2} \cdot \frac{32.2 \text{ lbm} \frac{\text{ft}}{\text{sec}^2}}{144 \text{ in}^2} \cdot \frac{\text{lb}_f}{\text{ft}^2}$$

$$= 5.14$$

Figure 2-5. (continued).



Upon completion of the nodalization process, including the documentation, the user should have an independent checker review the model to verify that all the numbers and assumptions are correct. The checking phase is quite important, particularly if the model is a simulation of a commercial plant and the planned calculations are intended as input for licensing or policy-making decisions. Consequently, the checker is chartered to independently verify every single number that was input to the model. After completing the checkoff process, the checker should be asked to sign each worksheet (Figure 2-5) to indicate the worksheets have been reviewed and all problems have been resolved.

### 2.2.3 Obtaining the Boundary and Initial Conditions

Following the nodalization phase, the model is fully defined (as shown in Figures 2-2, 2-3, and 2-4): all dimensions are known, the various model flow paths are defined and simulate comparable flow paths in the physical system, the system metal mass is simulated, the logic that defines valve openings and closures, pump behavior, etc. is known. The next steps consist of inputting the model to the computer, checking the input for errors and inconsistencies, and obtaining a steady-state system balance.

**2.2.3.1 Installing the Input.** The RELAP5 input is defined in Volume 3. The specific structure and user guidelines are described in Section 3 of this volume.

Although it is a straightforward task to copy the various inputs from the documentation (Figure 2-5) into a computer file, transcription errors are among the most common. Error messages are displayed if some dimensions are not compatible; however, the user should not depend solely on the code's error messages because many input items are not checked by the code's internal checking algorithms. Worthy of special mention is the code's ability to detect whether model loop elevations are "closed." For example, considering the model shown in Figures 2-2 and 2-4, a loop is formed by components 404, 405, 406, 408, 410, 412, 414, 416, 418, 420, 102, 104, 106, 110, 112, 114, 118, and 120. If the sum of the elevation changes within these components is not zero, then an artificial pump would be inadvertently present in the system model with a head equal to the hydrostatic pressure mismatch caused by the loop elevations. The code initialization logic is programmed to check for such mismatches.

**2.2.3.2 System Steady-State.** The system steady-state calculation is of particular importance in preparing for the transient calculation. The model steady-state condition is adjusted to match the physical system's initial condition.

The code contains a "steady-state" option to assist the user in reaching the correct initial conditions. Since the steady-state condition represents the initial fluid conditions and the metal mass initial conditions, the "steady-state" option enables the user to quickly reach steady-state thermally and hydraulically by reducing the specific heats of the metal masses to a low value. Thus, the model quickly converges to a condition representative of fluid conditions either input by the user or consistent with the user-input controllers. If reactor kinetics are also included in the model, the neutronics are often manually disabled until the system hydraulics have reached an unchanging steady-state condition to prevent formation of an unstable hydraulic-neutronics feedback system.



It is important that the user allows the model to run for a sufficient length of time before concluding that a steady-state condition has been reached. The user should ensure that a fluid particle moving from one part of the system can make a number of complete circuits back to its point of origin. Once a steady-state condition has been reached, the fluid conditions should be virtually unchanging with time. Such a condition is shown in Figure 2-6 for the steam generator steam and feedwater mass flow rates as calculated for the model shown in Figure 2-3. Following an initial mismatch between the two flow rates, after 60 seconds the steam flow out exactly matches the feed flow in, and the two flows are steady.

As for all other phases of the model-building process, each step and model adjustment should be documented in the problem description and solution notebook.

## 2.2.4 Running and Analyzing the Problem

The final phase of the solution process consists of running the problem on the computer and analyzing the results. This phase can be quite lengthy if the transient is complex.

**2.2.4.1 Running the Problem.** Running the problem on the computer is often thought by the novice user to be a trivial process. However, a number of difficulties may arise that may seem insurmountable at first glance. Two of the most common difficulties are

- Unexplained failures--Sometimes the code will fail and give a failure message that is not easily understood. For example, the code may give results showing unrealistic pressures or temperatures in one of the model nodes. The failure message would indicate that the code "was unable to converge." Such failures can sometimes be circumvented by reducing the time step by a factor of two or more and then resubmitting the job.
- Unexpected convergent results<sup>e</sup>--Often the user may be required to analyze a transient that is a variation of an analysis done by other users. If this is true and the new analysis results are unexpectedly different, the user should carefully reexamine the input boundary conditions. User-input errors cause equipment operations (e.g., valve operations, pump head increases or decreases, and power transients) that do not match the realistic system behavior.

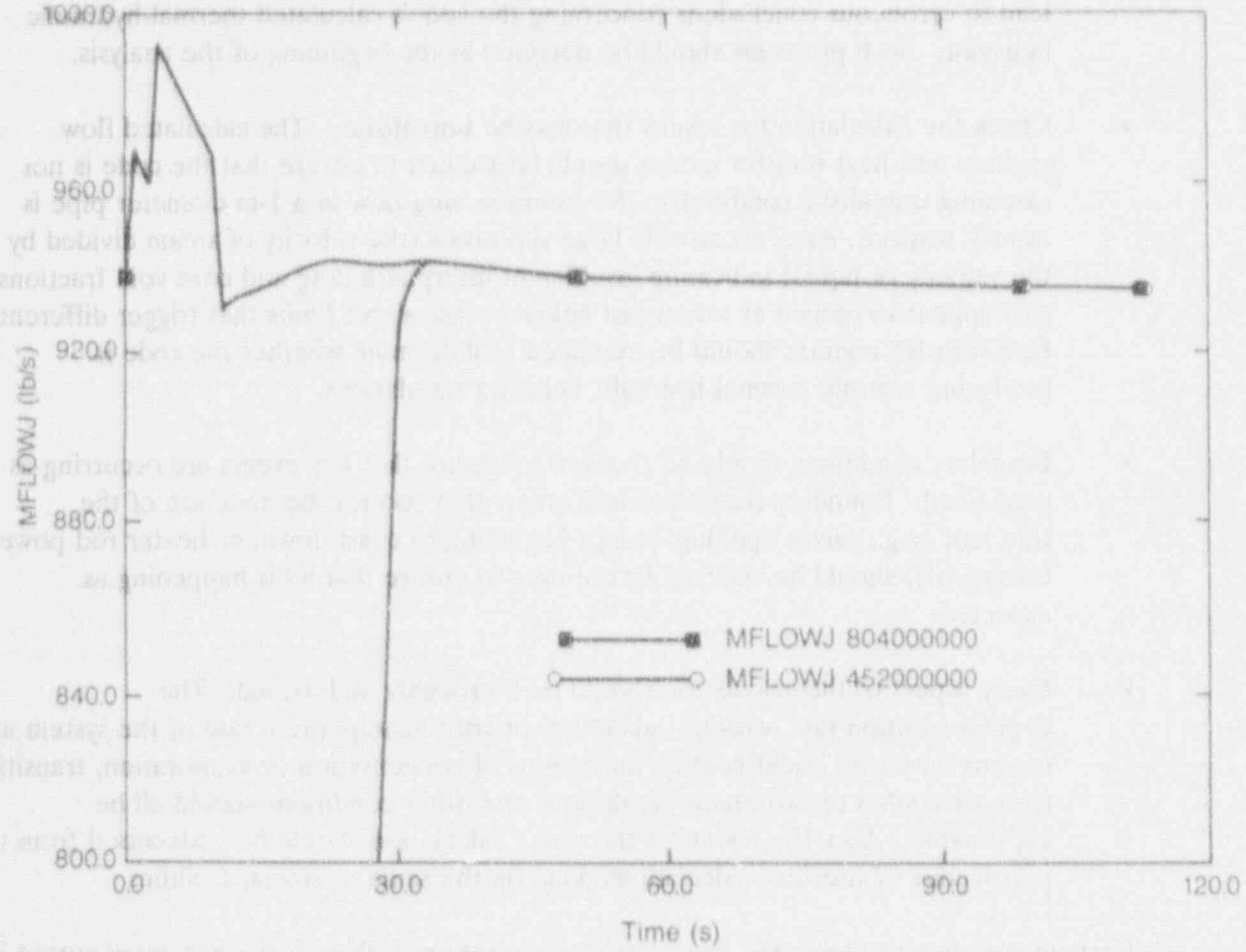
**2.2.4.2 Analyzing the Problem.** Analysis of the RELAP5 results is a methodical process that should be designed to

- Check the output for indications that the code did not converge properly. Such indicators include nonphysical state properties and excessive mass error. If the code did not converge numerically, error messages should be visible.

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e. Code output is said to be convergent when the same result is obtained regardless of the nodalization.

...the output for nonphysical results. ...  
 ...the output for nonphysical results. ...  
 ...the output for nonphysical results. ...



1-6979

Figure 2-6. Workshop problem steady-state with controllers (steam and feedwater mass flow rates).

- Check the output for nonphysical results. Results indicating liquid over steam (when vapor flow rates are not sufficiently large to cause counter-current-flow-limiting), prolonged existence of metastable thermodynamic states, and unphysical oscillations that could be numerically-induced are all examples of nonphysical results that may lead to erroneous conclusions concerning the code's calculated thermal-hydraulic behavior. Such problems should be detected at the beginning of the analysis.
- Check the calculation for results that may be unrealistic. The calculated flow regimes and heat transfer modes should be studied to ensure that the code is not assuming unrealistic conditions. For example, slug flow in a 1-m diameter pipe is usually suspect. Also, excessively large slip ratios (the velocity of steam divided by the velocity of liquid) indicating insufficient interphase drag and core void fractions that appear to remain at values just below or just above limits that trigger different heat transfer regimes should be examined to determine whether the code is producing realistic thermal-hydraulic behavior simulations.
- Boundary conditions should be checked to ensure that key events are occurring as prescribed. Boundary conditions and others that control the direction of the transient (e.g., valves opening, pumps beginning to coast down, or heater rod power turning off) should be checked by the user to ensure that all is happening as expected.
- Every aspect of the calculation should be thoroughly understood. The depressurization rate, various indications of core heatup, drain rate of the system at various locations, liquid holdup, indications of condensation or evaporation, transition from subcooled to two-phase break flow, and other conditions should all be explainable. Also, the results of the user's calculation should be understood from the perspective of previous calculations done on the same or similar facilities.

Early in the analysis phase, the user should use graphics so that all the necessary output is obtained. Also, the analyst should use RELAP5's minor edits whenever possible. Such diagnostics are invaluable during the analysis process for a thermal-hydraulic calculation.

Analyzing the RELAP5 results is one of the most important phases of the total analysis process. The first and foremost caution is that the user must never accept an answer from the code without first asking whether the result seems reasonable. A thorough examination of the code output for each analysis is a cardinal rule that must never be violated. The user must evaluate whether each and every trend shown by the calculation is consistent with the boundary conditions, the initial conditions, and the known behavior of a simplified representation of the problem.

## 2.3 Basic RELAP5 Modeling Units

The process of building a RELAP5 model can be envisioned as analogous to physically building the system that is being modeled. Just as the physical system is composed of pipes that are connected by welded or bolted flanges, valves, pumps, and other components, so is the

RELAP5 model. Although a few of the RELAP5 building blocks are specialized (e.g., the PUMP component and the VALVE junction), most are general purpose.

The RELAP5 building blocks can be divided into four fundamental groups: thermal-hydraulic, heat structures, trips, and control variables. The thermal-hydraulic group is composed of components designed to simulate fluid passages and fluid-handling equipment. Heat structures are designed to simulate material mass and the interactions between the material mass and the fluid in the fluid passages. Trips are designed to simulate the signals that initiate equipment actions of various sorts (e.g., turning on a pump at a desired time or causing a valve to open at one pressure but close at another pressure). Finally, control systems are designed to give the code model added capability by allowing equipment control systems (e.g., proportional-integral-differential controllers and lead-lag controllers) and "lumped-node" systems to be simulated. The basic building blocks for the thermal-hydraulic and control variable groups are listed in Tables 2-1 and 2-2 respectively.

### 2.3.1 Thermal-Hydraulic Group

Within the thermal-hydraulic group there are ten fundamental RELAP5 components that can be grouped by function. General components that are used for simulating stream-tube volumes are the single-volume component, the pipe or annulus component, and the branch component (including the separator, jet-mixer, turbine, and emergency core cooling mixer components). General components that are used to provide stream-tube connections from one component to another are the single-junction component and the multiple-junction component. Components designed to simulate boundary conditions are the time-dependent volume component and the time-dependent junction component. Components designed to simulate particular equipment are the valve component, the pump component, and the accumulator component. Each of these components is listed in Table 2-1. If more detailed information is required, consult Section 4.

### 2.3.2 Heat Structures

The heat structure modeling capability inherent to the RELAP5 code allows simulation of all of a system's material mass. System structures constructed of different types of materials (e.g., a cast iron pipe covered externally with insulation and plated on the inner diameter with stainless steel) can be modeled easily using the code. Also, the code can simulate the presence of heat sources within heat structures such as nuclear fuel or electrical heating elements.

The heat structures simulate the behavior of not only the core fuel rods in a reactor system, but also the various plant structures. Thus, the heat structures simulate both energy storage in the material mass and energy transfer to or from the material mass to the fluid in the simulated stream-tubes. Energy storage and transfer in the heat structures is calculated by the code using a geometry defined by the user; each heat structure is sized to interact with particular stream tubes and each heat structure can be finely nodalized to provide a rather detailed temperature distribution in one dimension. A plane slab structure, a cylindrical structure, or a spherical structure is allowed for each slab. The code assumes that energy flow to and from the heat structures is in a direction normal to the stream-tube flow direction. Consequently, the heat

**Table 2-1.** Summary of the RELAP5 thermal-hydraulic building blocks.










Component	Label	Schematic	Primary Uses
Single-volume	SNGLVOL	 <sup>a</sup>	Represents a portion of stream tube that doesn't require PIPE or BRANCH.
Pipe or annulus	PIPE	 <sup>b</sup>	Represents a pipe in the system. PIPE can have 1 to 100 subvolumes. PIPE with more than 1 subvolume has internal junctions connecting the subvolumes.
	ANNULUS		Special form of PIPE. Has the same characteristics as PIPE but is used to simulate annular flow passages.
Branch	BRANCH	 <sup>c</sup>	Represents a stream tube flow juncture that can have as many as 10 junctions defined.
	SEPARATR		Special form of BRANCH that simulates a water separator in a steam generator.
	JETMIXER		Special form of BRANCH that simulates a jet pump.
	TURBINE		Special form of BRANCH that simulates a steam turbine.
	ECCMIX		Special form of BRANCH that simulates a stream tube flow juncture with a potential of large condensation rates.
Single-junction	SNGLJUN		Designed to connect one component to another.

Table 2-1. (continued).

Component	Label	Schematic	Primary Uses
Multiple-junction	MTPLJUN		Connects components to other components (up to 100 connections allowed).
Time-dependent volume	TMDPVOL		Specifies boundary conditions on system model.
Time-dependent junction	TMDPJUN		Connects one component to another and specifies junction boundary conditions concurrently.
Valve	VALVE		Simulates the actions and the presence of six different valve types: check, trip, inertial, motor, servo, and relief.  The valve component is a special junction component.
Pump	PUMP		Simulates the actions and presence of a centrifugal pump.
Accumulator	ACCUM		Simulates a PWR accumulator.  Model includes not only the vessel, but also the accumulator surge line.

a. Junction.

b. Volume.

c. Junction connecting two adjacent volumes.



**Table 2-2.** Summary of RELAP5 control variable building blocks.

Component	Label	Function
Sum-Difference	SUM	Allows addition or subtraction of variables
Multiplier	MULT	Allows multiplication of variables
Divide	DIV	Allows division of two variables
Differentiating	DIFFRENI or DIFFREND	Performs differentiation of a variable as a function of time
Integrating	INTEGRAL	Performs integration of a variable as a function of time
Functional	FUNCTION	Defines a table lookup functional relationship to a variable
Standard Function	STDFNCTN	Performs absolute value, square root, exponential, natural logarithm, sine, cosine, tangent, arc-tangent, minimum value, or maximum value operation on designated variable
Delay	DELAY	Acts as a time delay factor operating on designated variable
Unit Trip	TRIPUNIT	Becomes true at defined time (when true = defined factor, when false = 0); also can be defined as complementary function
Trip Delay	TRIPDLAY	Becomes true at defined time (when true = trip time $\times$ factor, when false = -1)
Integer Power	POWERI	Gives variable raised to integer constant power I quantity times constant
Real Power	POWERRR	Gives variable raised to real constant power R quantity times constant
Variable Power	POWERX	Gives variable raised to real variable power V quantity times constant
Proportional-Integral	PROP-INT	Defines a proportional-integral controller

Table 2-2. (continued).

Component	Label	Function
Lag	LAG	Defines a lag controller function
Lead Lag	LEAD-LAG	Defines a lead-lag controller function
Constant	None	Defines a constant value to be used with other control variables
Shaft	SHAFT	Defines shaft characteristics that may be used in conjunction with a generator
Pump control	PUMPCTL	Defines a pump controller (used principally during steady-state portion of analysis)
Steam control	STEAMCTL	Defines a steam flow controller (used principally during steady-state portion of analysis)
Feed control	FEEDCTL	Defines a feedwater flow controller (used principally during steady-state portion of analysis)

structure nodes are aligned in the direction normal to the fluid flow. A comprehensive description of the RELAP5 heat structure nodalization process is given in Section 4.

### 2.3.3 Trips and Control Variables

The trip capability available in the RELAP5 code enables the user to specify actions during a simulated system transient. When coupled with the code's control variables, the user has a versatile tool that greatly expands the capabilities of the RELAP5 code.

The trip logic can be used with the time-dependent volume component, the pump component, the valve components, the time-dependent junction component, some options of the branch component, the accumulator component, and with tables used to describe reactor kinetics characteristics and heat structure characteristics. In general, the trip's condition is either true or false. The trip's condition is determined at each time step by checking the status of the trip-defined test. The test consists of comparing the specified variable to either another variable or a parameter using specified conditions such as equal to, greater than, less than, greater than or equal, less than or equal, or not equal. In combination with the "logical trips," very complex logical sequences can be simulated since the "logical trips" allow comparison between two or more trips such that one or more trips may be required to be true to create a true "logical trip" condition. A detailed description of the trips is given in Section 4.

The code's control variables consist of 21 capabilities (see Table 2-2). In essence, the control variables can be used for three primary functions: (a) to simulate equipment control systems, (b) to create "lumped node" parameters, and (c) to add further dimensions to the boundary conditions imposed on the thermal-hydraulic group and heat structure group components.

**2.3.3.1 Simulating Equipment Control Systems.** Every piece of equipment that is a component of a physical system has a control system. The control system may be no more sophisticated than a simple on/off switch that is controlled by the equipment operator. Sometimes, however, equipment control systems can be highly complex and sophisticated. Consequently, the code has control variable components designed to allow the user to model virtually any physical component of the equipment system. Specifically, the lag, lead-lag, proportional-integral, and differential components are designed to simulate common controller functions. When used in combination with the other control variable components, even the complex and sophisticated Babcock & Wilcox's (B&W's) PWR Integrated Control System has been successfully modeled using RELAP5.

**2.3.3.2 Simulating "Lumped Node" Systems.** Equipment components such as containments, tanks, flow systems, and balance-of-plant components can be simulated using the control variables by creating difference equation sets that represent the specific component's behavior. The equation sets can then be coupled to the RELAP5 model of primary interest using tables and simple functional relationships to simulate the interactions between the primary thermal-hydraulic model and the "lumped node" models.

**2.3.3.3 Enhancing the RELAP5 Model Boundary Conditions.** The control variables can be used to simulate the presence of instrumentation that provides key input to system trip cri-

equipment functions. For example, a piece of instrumentation affected by the total pressure rather than the static pressure can be modeled by creating a control variable that monitors the fluid static pressure and the fluid velocity head to calculate the total pressure head (in the absence of a gravitational change), and then provides a value to be compared to a trip test value. Similarly, the critical flow energy flux can be calculated using the control variables to determine the flow enthalpy at each time step (since RELAP5 only calculates the flow specific internal energy, not the specific enthalpy).

## 2.4 Basic RELAP5 Modeling Guidelines

Using the building blocks described in the previous section, the model shown in Figures 2-2 through 2-4 was constructed. The model uses eight of the ten components available in the thermal-hydraulic group together with heat structures. Trips are used to change the operational state of the valves, the pump, the pressurizer heater rods, and the core power level as a function of the following variables:

- Primary inventory level (pressurizer water level)
- Secondary inventory level
- Primary and secondary pressures
- Hot and cold leg temperatures.

A summary of the basic guidelines and their applications are given in the next three subsections to illustrate the first steps in constructing a RELAP5 model.

### 2.4.1 Simulating the System Flow Paths

The flow paths shown in Figures 2-2 through 2-4 were nodalized by adhering to the following general rules:

- The length of the volumes is such that all have similar material Courant limits.
- The volumes have a length-to-diameter ratio greater than or equal to 1 with the exception of the bottom of the pressurizer (see component 341, volume 7 in Figure 2-2). The volume representing the bottom of the pressurizer was sized to have a length-to-diameter ratio less than 1 to allow better definition of when the pressurizer empties during an LOCA.
- A nodalization sensitivity study was undertaken to determine the best model representation. Thus, several different nodalizations of the steam generator U-tubes were studied.
- Portions of the model containing a "free surface" were nodalized such that the "free surface" lies approximately midway between the node boundaries. Thus, the normal pressurizer water level is approximately at the middle of component 341, volume 2.

- Unnecessary flow paths were eliminated. Therefore, even though there are eight to ten flow paths between the vessel downcomer (components 100 and 102) and the vessel upper head and upper plenum (components 126, 122, and 120), only two paths were simulated (junctions 12601 and 10203). All the small flow paths were simulated by these two flow paths.

#### 2.4.2 Simulating the System's Heat Structures

A system's heat structures should be simulated if there will be interactions between the heat structures and the fluid stream-tubes. Circumstances leading to such interactions occur because of

- The presence of power sources (energy sources) located in heat structures.
- Large fluid temperature changes. For example, if a system is initially at 1000 psia and a large valve suddenly opens such that the system depressurizes rapidly, the fluid temperature will follow the saturation temperature during the depressurization. Consequently, the heat structures, at the initial fluid temperature, will then transfer energy to the fluid in an effort to reduce the heat structure to fluid temperature potential.
- Environmental losses. Although commercial plants have thermal losses to the environment that represent only a small percentage of core decay heat, scaled experiments may have losses that are large compared to simulated core decay heat.
- Primary to secondary energy transfer in heat exchangers, steam generators, etc. A typical commercial PWR provides steam to the power turbines by boiling secondary inventory using energy supplied by the primary core fuel rods.

Based on the above guidelines, the heat structures for the one-loop model shown in Figures 2-2 through 2-4 were constructed. The reader should note that the majority of the structural materials were simulated including the reactor vessel walls, the steam generator vessel walls, the steam generator U-tubes (heat structure number 1081), the reactor core (heat structure number 1141), and the pressurizer heater rods (heat structure numbers 3411 and 3421).

#### 2.4.3 Trips and Control Variables

The actions and/or response of the model's simulated equipment is triggered and sometimes controlled by the trips and control variables. Thus, the following equipment has trips and sometimes control systems that guide its behavior during off-normal conditions:

- Pressurizer heaters (heat structures 3411 and 3421)
- Core (heat structure 1141)
- Pressurizer spray (valve component 338)

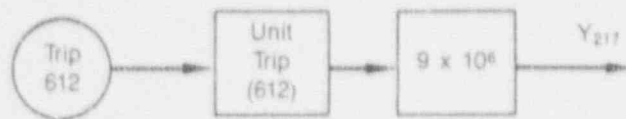


- Pressurizer safety valve (valve component 346)
- Power-operated relief valve (valve component 344)
- Reactor coolant pump (pump component 414)
- Primary fill system (time-dependent junction component 972)
- Secondary steam system valves (valve components 755, 765, and 804)
- Feedwater system (time-dependent junction component 455).

As an example, the control system and governing trips for the on/off pressurizer heater (heat structure 3421) is shown in Figure 2-7. The parameter labeled  $Y_{217}$  is the heater rod power in MW.  $Y_{217}$  equals 0 when trip 612 is false and equals 0.9 MW when trip 612 is true. The logic works because the unit trip equals 0 when trip 612 is false and equals 1 when trip 612 is true. The trip logic, shown in the table below the controller logic, shows that the state of trip 612 is based on the state of trips 611, 510, 511, and 512. Trips 510, 511, and 512 are called variable trips and trips 610 and 611 are called logical trips. Trip 510 states that when controller 510 (an indication of the pressurizer liquid level) is less than or equal to -3.144, the trip becomes true and it is then always latched open. Trip 511 states that when the hot leg to cold leg temperature difference bias (represented by controller 203) is less than -0.05, the trip becomes true and only remains true as long as that condition is maintained (i.e., the trip is not latched). Trip 512 states that whenever the primary system pressure bias is less than or equal to -25 (controller 212), then the trip is true and the trip is not latched. If either trip 511 or trip 512 is true, then trip 611 is true, but not latched. Finally, if trip 611 is true and if trip 510 is *not true* (represented by the -510), then trip 612 is true.

Although the logic for having the pressurizer on/off heater is simple, five trips were required to program all the conditions that must be satisfied prior to having the heater on. An elaborate system can have hundreds, or even thousands, of controllers and trips.





Trip	Parameter	Operator	Constant	Latch or no latch
612	611	.A'	-510	N
611	511	OH	512	N
510	CONTRVAR 202	.LE.	-0.144	L
511	CONTRVAR 203	.LT.	-0.05	N
512	CONTRVAR 212	.LE.	-25.	N

1-6978

Figure 2-7. Pressurizer heater rod controller: on-off (component 3421).

## 3. GENERAL PRACTICES

This section discusses general practices for applying RELAP5 including standard procedures, calculational node and mesh sizes, options, and special model applications.

### 3.1 Standard Procedures

Standard procedures for input preparation, debugging the model input, problem execution, and output interpretation are presented in this section.

#### 3.1.1 Input Preparation

Attention to detail in preparing, documenting, and checking the input limits errors and provides a valuable model reference for tracking error corrections and subsequent model improvements. By using standardized input format and conventions, input errors are easier to detect. The following sections discuss standard procedures for model documentation and quality assurance, input deck arrangement, and conventions.

**3.1.1.1 Model Documentation and Quality Assurance.** The primary tool for RELAP5 model quality assurance is the model workbook. The references, assumptions, and calculations needed to generate the code input are assembled into a workbook that is retained and controlled. A formal requirement to produce a model workbook forces a discipline on the modeler that reduces the possibility of errors. Furthermore, formally requiring the written data in the workbook to be certified forces a discipline on an independent checker.

A typical workbook might begin with discussions of the purpose for the model, general facility references, the scope of the model, top-level assumptions, and relation to existing models. Next, an overall model nodalization scheme is developed and documented in the workbook. The nodalization numbering scheme should be carefully considered; logical numbering of various modeling regions greatly facilitates error detection and output interpretation. As an example, a logical scheme for a three-loop pressurized water reactor might number the components in the loop 1 region from 100 to 199, loop 2 from 200 to 299, and loop 3 from 300 to 399. Reactor vessel components might be numbered 400 to 499, pressurizer components 500 to 599, feedwater and steam systems 600 to 699, and additional systems (e.g., makeup, letdown, safety injection, accumulators) 700 to 799. Numbering scheme symmetry should be used where possible. In the above example, if component 120 represents the hot leg in loop 1, then components 220 and 320 would represent the hot legs in loops 2 and 3, respectively.

A minor consideration, but one that can prevent misinterpreting the output, is to avoid numbering components from 1 to 99. Plotted and tabulated code output is referenced by component or cell number with four zeros appended (e.g., the pressure in branch 120 is referenced P 120010000). The digits represented by the appended zeros were included to provide a means of referencing a multidimensional component. Although this multidimensional capability was never incorporated into the code, input and output functions still use the trailing zeros. By limiting component numbering to numbers from 100 to 999, all component references are standardized at 9 digits (three for component, two for cell, and four trailing zeros). The

advantage of this approach is that the possibility of misreading component numbers in the output is avoided. For example, if component numbers from 1 to 99 are used, then on casual inspection an indicator 120010000 may be visually mistaken for 12010000 (the first for component 120, the second for component 12). If all component numbers are 100 or larger, then there is no ambiguity because the first three digits of the indicator are always the component number.

The main portion of the model workbook contains worksheets to document the information needed to assemble the code input. The workbook is typically assembled in an order consistent with the component numbering. For each component, the hydrodynamic data are typically documented first, followed in turn by the heat structure data and control system data. It is useful to tabulate component data in the order that it is to be input. (The tables can include page number references to the location of each input parameter.) This greatly reduces the effort required to enter the code input parameters. A sample workbook page is shown in Figure 3-1. For each model component the workbook documents (a) the sources of information used to assemble the model (such as drawing and report numbers), (b) assumptions, (c) any calculations needed to convert the raw data, and (d) the final values of the code input parameters.

When completed, the workbook is used directly to key-enter the code input parameters into a computer file for the model. Diligence should be used at this stage of the process since key-entry errors are likely. Experience has shown that the careful entering of each number and a detailed comparison of the resulting computer file and workbook are worthwhile efforts. While this effort is intensive, it is needed to prevent serious errors such as mis-specifying input by orders of magnitude.

At the INEL, it is a standard quality assurance practice that each input model be independently checked by an engineer other than the one who developed the model. Independent checking involves certifying all aspects of the model development process: verifying references, considering the appropriateness of the assumptions, double-checking the hand calculations, checking the units, and confirming the translation of the data to the computer file. Any anomalies found during the checking process are resolved between the model developer and checker, and the model is modified accordingly. The model workbook is signed and certified by both the developer and checker.

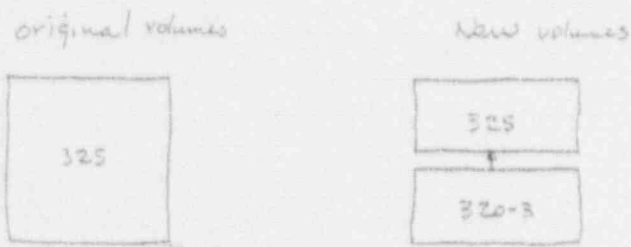
The independent checking activity is perceived by many engineers (especially senior engineers) as tedious, uninteresting work. As a result, the checking function tends to fall to junior engineers. Junior engineers prove capable of certifying the details of a project but may be incapable or unwilling to challenge top-level modeling decisions and assumptions. In the authors' opinion, the independent checking function pays significant quality assurance benefits both in avoidance of costly errors and in the ultimate confidence of analysis results. To be effective, senior engineers must recognize that the benefit of checking is well worth the tedium of the effort required and approach the task positively. Junior engineers must recognize that, as independent checkers, it is important they concur with or question the top-level assumptions.

CALCULATION WORK SHEET

Page 8 of        Pages

Subject Sensitivity 1, SG Normalization Study Date July 5, 1985  
 Prepared By M.A. Bolander Checked 7-30-85 (CD) Work Request       

Take volume 325 (shown on page 2) and divide it in half.



The original length of 325 is 7.906 ft (work book page 79)

Volume is 338.938 ft<sup>3</sup>

From the lower tube sheet to the upper tube sheet the distance is 52.0312 ft (work book page 67)

The upper grid spacer is 48.250 ft from the lower tube sheet.

The length of the new 325 and 320-3 volumes =  $\frac{1}{2}(7.906) = \underline{\underline{3.9530 \text{ ft}}}$

Locate the upper grid spacer:  $52.0312 \text{ ft} - 3.9530 \text{ ft} = 48.0782 \text{ ft}$

The grid spacer physically is at 48.250 ft. Assume the grid spacer sits

in volume: 325. Therefore there is 1 grid spacer in volume 325

and 1 grid spacer in volume 320-3.

Volume of New 325 =  $(43.117)(3.9530) + \pi(5.0573^2 - 4.9323^2)(1.0938) - \frac{6.2356}{2} = \underline{\underline{171.644}}$   
 Refer to: work book pages 71, 72, 79

Figure 3-1. Sample model workbook page.

**3.1.1.2 Input Deck Arrangement.** The code accepts data based on the "card number" specified in the first field on each line of input. For a given card number, the code accepts the input parameters specified in the code manual as sequences of floating point, integer, and alphanumeric entries. On any given card, the data entries must appear in the proper sequence and be separated by one or more blanks. The cards may appear in any order, as long as all required cards and data entries are present. If a card number is duplicated in the input listing, the code identifies it as a "replacement card" and uses the information on the last card entered with that number.

A well-organized input deck includes comment cards that aid interpreting the input from a printed listing. Comments may be inserted through the use of the asterisk (\*). On any line, all entries following an asterisk are assumed to be comments. An example of a fully-commented input listing is shown for a branch component in Figure 3-2. With this format, an analyst will spend a minimum amount of time counting fields and searching through the manual to understand the input.

As stated above, the input deck cards may appear in any order. In practice, however, arranging the cards in a logical manner is preferred. At the INEL, input decks typically start with the title, job control, and time step control cards. These are followed in sequence by the minor edit requests, trip specifications, hydrodynamic components, heat structures, user-input data tables, control variables, and reactor kinetic specifications. An input deck is generally arranged by increasing card numbers when this arrangement is used. Within each of the above groups, data are similarly arranged in order of the card numbers (e.g., the trips are listed in numerical order).

**3.1.1.3 Conventions.** The benefits of a logical numbering scheme for model components were described in Section 3.1.1.1. Similar benefits can be gained from a logical numbering scheme for heat structures and control variables.

For heat structures, benefits may be gained by assigning heat structure identifiers consistent with the hydrodynamic volumes with which they are coupled. Heat structures are referenced by the heat structure/geometry number (CCCG); for each heat structure, any CCCG may be selected. If, however, the CCC digits correspond with associated hydrodynamic volumes, interpretation of the output is enhanced because only one numbering scheme needs to be remembered. As an example, consider a pressurizer that has been modeled with 8-cell pipe 620. The hydrodynamic volumes are thus numbered 620010000, 620020000, ... 620080000. For the heat structures representing the pressurizer shell, a heat structure geometry number of 6201 would be selected, and 8 individual heat structures would be developed and connected in turn to cells 620010000 through 620080000. The advantage of this method would be that in the output heat structure, 6201005 can be easily associated with the pressurizer wall adjacent to the fifth hydrodynamic cell of the pressurizer. Where it is required that more than one heat structure be connected to the same volume, the above convention may be extended by using the same CCC but increasing the G. In the above example, a heat structure for a pressurizer heater might be identified with a CCCG of 6202.

For control variables there is a similar benefit to be gained by selecting control variable numbers consistent with a representative component. In the above example, the control variables associated with the pressurizer heaters and spray system might be numbered 610 to 620. The user

```

$.....$
*hydro      component name      component type
1150000    "hxinplen"                    branch
-----$
*hydro      no juns              vel/flw
1150001    2                            0
*
*hydro      area                  length                volume
1150101    0.                            1.065                1.265
*
*hydro      horz angle                vert angle            delta r
1150102    0.                            0                    0
*
*hydro      roughness                  hyd diam              fo
1150103    0.0000457                    1.265                00
*
*hydro      ebt pressure              tempe                2414206 0
1150200    0 1808064.                    332978.
*
*hydro      from                to                area                f loss                r loss                vcahs
1151101    110010000          115000000          0                    0                    0                    00100
1152101    115010000          120000000          0                    0                    0                    00100
*
1152110    0 01412 0 1 1.
*
*hydro      f flowrate                g flowrate            j flowrate
1151201    9.03925                9.03925                0 * 809.737
1152201    2.111856                2.111856                0 * 804.918
$.....$

```

Figure 3-2. Example of full-commented input for a branch component.



is cautioned, however, that the control variable numbering scheme must consider that control variables are evaluated in numerical order during each time step. If control variable 623 refers to control variable 620, the new time value of control variable 623 is used. However, if control variable 620 refers to control variable 625, then the old time value of control variable 625 is used.

As a general convention, it is advantageous to define positive junction directions consistent with flow during normal operation of the system. With this technique, indications of positive junction flow (positive mass flow rates and velocities) in the output can be considered normal by the analyst. More significantly, the appearance of negative junction flow (indicated by minus signs) can be an indicator highlighting unusual behavior to the analyst. The sense of the junction flow is defined by the "FROM" and "TO" hydrodynamic cells specified. "FROM" to "TO" cell flow is considered to be positive.

The user does not have the capability to change the direction of positive heat transfer. The code convention on each surface of a heat structure is that the flow of heat from the structure to the fluid is positive. As an example, consider the heat structure of a steam generator tube. The left side of the structure is connected to the primary coolant system; the right side of the structure is connected to the secondary system. During normal operation, with heat flowing from the primary to the secondary, the heat transfer (rate and flux) on the left surface is indicated as negative while it is positive on the right surface.

The user does, however, have the option of specifying either the left or right surface of a heat structure as the inner surface (in cylindrical and spherical geometries). It is advantageous, but not necessary, to make this decision consistently. At the INEL, the convention is to assign the geometrical inner surface as the left surface and the geometrical outer surface as the right surface. For example, cylindrical pipe walls are modeled with the inner/left surface adjacent to the fluid within the pipe and the outer/right surface representing the outside of the pipe. For fuel rods, the left surface represents the centerline of the rod (specified as an adiabatic boundary) and the right surface represents the outside of the cladding.

Extended trip and control variable capabilities have been included in the code and the user has the option in each case to select the original or extended capability. Note, however, that all trips and all control variables in a problem must conform to the option selected. These extended capabilities were included as the size of control system models outstripped the originally-defined limits on the number of control variables and trips. For new models, selecting the extended options is recommended to allow greater capability for adding to the model.

### 3.1.2 Model Input Debugging

The input processing routines provide excellent error-checking and error-interpretation capabilities. Input processing error checking is invoked when executing both new- and restart-type problems. All model input errors result in the generation of an informative error message. The presence of one or more input errors results in job termination and a message that the termination was due to input error. As a word of caution, the RELAP5 error-checking functions are primarily intended to check for compliance with the input data requirements. Secondly, checking is performed for model consistency (e.g., that elevations are consistent around flow loops). However, the input error-checking function may not uncover basic input errors such as

mis-specifying a volume of  $10 \text{ m}^3$  as  $1000 \text{ m}^3$ . Therefore, successful completion of RELAP5 input processing should not be considered a replacement for the quality assurance activities described in Section 3.1.1.1.

Optional job control card 101 provides a capability to automatically terminate a job following input processing. If the INP-CHK option is specified, all input processing functions are performed and the initial time major edit is generated, but no transient calculation is performed. If the RUN option is selected, the input processing is performed, the initial time major edit is generated, and the transient calculation is initiated. If card 105 is not input, the RUN option is assumed.

An efficient method for debugging a new RELAP5 input deck is described as follows. The complete model is first assembled into a single file and the model is executed in either the transient or steady-state modes as specified on card 100. Either the INP-CHK or the RUN option may be selected on card 101. A typical new input deck will likely contain many input errors so the execution will result in generation of a series of error messages. It is common for one actual error to propagate into the generation of multiple error messages. Therefore, the list of error messages generated will in general be much longer than the actual number of errors in the model. The user should read and consider each of the error messages in the order they were generated. This process results in one of the following determinations for each of the error messages: (a) the message clearly indicates an error in the deck and the resolution is clear, (b) the message is found to be caused by the existence of a previous error and is expected to be resolved when the primary error is corrected, and (c) the reason the message was generated is not clear. In practice, the error messages are very informative and the actual input errors are obvious to the analyst. A significant effort can be expended tracing the source of each error message. Instead, it is more efficient to survey the error messages, correct the obvious errors, and again execute the model. As a rule of thumb, only about one third of the error messages generated are caused by actual errors; the remainder are second-generation messages resulting from the primary errors. This iterative process proceeds rapidly to the removal of all input errors. Experience shows that a large input deck that has been entered with moderate care can be debugged with this process in about five iterations.

The iterative debugging process described in the previous paragraph can be much easier if the output of the debugging runs are reviewed on a terminal by an editor capable of searching for data strings. All input error messages are preceded by a string of eight asterisks (\*\*\*\*\*\*) and the removal of all errors results in the generation of the message "input processing completed successfully."

The user should be aware that the input processing is subdivided into several sections of data checking that are performed in sequence. Depending on the nature of the errors found, the job may be terminated at the end of one of the sections before all of the error-checking sections have been executed. In this instance, only error messages for the sections that have been checked will appear. When these errors have been corrected and the checking proceeds to the next section, the number of error messages may increase. In other words, the analyst should realize that in this iterative process the number of error messages may not monotonically decrease.

As a part of the input processing routine, the elevation closure of all flow loops in the model is checked. An input processing failure message is generated if any of the flow loops fail to close elevation by more than 0.0001 m. Following such a failure, the elevation closure edit data may be examined to find the source of error.

A spurious input processing failure has been encountered by some users and is usually reported as a code execution failure occurring immediately after input processing has been completed. The diagnostic print-out states an arithmetic error or arithmetic overflow has occurred. The most common source of this error is the inadvertent specification of a non-condensable gas in the system. This error is created when the user specifies an incorrect value for the initial condition control word. Control words of 4, 5, and 6 are reserved for mixtures with a non-condensable gas; the error occurs if any of these control words are used when a non-condensable gas has not been specified on card 110.

### 3.1.3 Problem Execution

When the input deck has successfully passed input processing, an initial time edit will be generated by the code. If the RUN option is selected, problem execution proceeds from the conditions specified in the initial edit. The initial edit will be identified as zero time for NEW problems and as the time of the restart edit for RESTART problems.

**3.1.3.1 Time Step and Edit Selections.** The problem execution is controlled by the options specified on the 201-299 time step control cards. These cards specify the time step sizes and output features desired as the problem progresses from one time interval to the next. Card 201 specifies these options and the end time for the first time interval, card 202 for the second time interval, and so on. Subdividing the problem into time intervals facilitates modifying the execution to suit the expected nature of the problem. For example, consider the case of a modeling action (such as closing a valve or tripping a pump) that is of particular interest and may slow the calculation at a given time (say 10 seconds). For this case, a first execution interval might be selected to end at 9 seconds. The second interval might include a reduced time step, and perhaps increased edit and plot frequencies, from 9 to 15 seconds. After 15 seconds, a third interval would then be used to return the time step and edit options to their original values. Note that execution is terminated if the problem time reaches the end of the last interval specified on the 201-299 cards.

For each time interval, minimum and maximum time steps are specified. The code will attempt to execute the problem at the maximum time step. The first time step taken will be at the maximum value. The user is cautioned to use a small maximum time step size when first executing a model for which gross approximations of initial conditions have been specified. Time step size is automatically reduced based on a number of tests. The material Courant limit may not be violated. Mass, fluid property, quality, and extrapolation errors are monitored in each calculational cell and the time step is reduced if errors exceed internally preset limits. The major edit output indicates the criteria and model region causing time step reduction. This indication can be useful for improving model performance.

The code accomplishes time step reductions by repeated division by two until the errors are within acceptable limits, the minimum time step size is reached, or a failure is encountered. The

user should note that this reduction process will result in running near the Courant limit only if the maximum time step size is appropriately selected. As an example, consider a problem where a 0.1-second maximum time step is specified and the Courant limit is 0.09 seconds. If not reduced for other reasons, the code will start with the 0.1-second maximum and repeatedly divide by two until a time step less than the Courant limit is attained. In this example, the code will execute the problem at 0.05 seconds, a much smaller time step than the 0.09-second Courant limit. Run time efficiency may be improved in the example by specifying a maximum time step size that is smaller than the Courant limit,  $\Delta t = 0.085$  seconds.

Frequently, when a calculation is running at a particularly slow pace due to time step size reduction, the selection of a smaller maximum time step size improves the progress of the calculation. This situation occurs when the specified maximum time step size is unacceptably large for the problem. When calculational difficulties are encountered, the code reduces the time step size. With the reduced time step, the code calculates through the difficulties and begins to recover. However, as recovery occurs the time step size is increased and the difficulties recur. Thus, reducing the maximum time step size prevents recurrence of the difficulties and improves the overall progression of the calculation.

It is not possible to formally recommend generally-applicable minimum and maximum time step sizes. These selections should be made considering the peculiarities of the code model, the problem to be solved, and the findings of any studies investigating the effect of time step size on calculation results. Furthermore, an appropriate time step size will vary during the course of a transient calculation as the calculated phenomena change. As a practical but informal guide, the user should consider using a minimum time step size of  $1 \times 10^{-7}$  seconds and a maximum time step size of the Courant limit (but not greater than 0.2 seconds). While a smaller minimum may be needed in some situations, if the above limit proves unsatisfactory it is usually an indication of significant calculational problems. The calculated phenomena should be carefully considered before proceeding. While it may be possible to execute a problem at very large time steps, the analyst should carefully evaluate the effects of large time steps in the context of representative model phenomena time constants and loop transit times.

The time step control cards contain a packed word (ssdt) specifying the code output format. The user is referred to the code manual for details regarding options. Generally, the option 00003 (or simply 3) should be selected. For persistent code failures (i.e., those that are not remedied by revision of time step size), problem diagnosis may be aided by obtaining a major edit at every time step as the problem is approached. This selection is made by the option 00103; obviously, care should be exercised to limit the size of the output file.

The minor, major, and restart edit frequencies are also specified on the time step control cards. These frequencies are specified as integer multipliers of the maximum time step size. For example, with a maximum time step of 0.1 seconds, a minor edit frequency of 10, a major edit frequency of 100, and a restart frequency of 200, the code will generate minor edits every 1 s, major edits every 10 s, and restart points every 20 s. In addition, the code generates minor, major, and restart edits at the initial problem time and at the end times for each of the 201-299 cards. If a transient code failure occurs, the code also generates these edits at the time of the failure and will designate the failure edit as a nonstandard edit. While review of the failure edits usually is quite valuable for understanding the failure mechanism, the user should not use the



failure edit as a restart point following correction of errors. For this purpose an appropriate (usually the preceding) restart time should be used.

The selection of the minor edit frequency is particularly important because the restart/plot output file will contain data points with the same frequency.<sup>a</sup> Once a calculation is performed, it is not possible to recover the data between these data points. Data for virtually all calculation parameters (pressures, temperatures, void fractions, flow rates, etc.) are available on the restart/plot file. A common misconception is that a parameter needs to be specified using a minor edit request in order to be available in the output when the calculation is complete. A minor edit request affects only the printed output. It is not necessary to specify all parameters needed for output in advance; this determination may be made after the calculation has been completed. The output file may be accessed repeatedly as new data needs arise.

It is recommended the user select minor edits for an appropriate plot output frequency, major edits for an appropriate phenomena snapshot frequency, and restart edits for an appropriate backup following failure frequency.

**3.1.3.2 Steady-State, Transient, and Strip Modes.** A calculation may be executed in the steady-state, transient, and strip modes as specified on control card 100. In the steady-state mode, the thermal capacitances of all heat structures are artificially reduced to speed problem response time; execution is terminated when internal tests for rate of change in parameters are satisfied. As a general recommendation, the steady-state mode is not recommended; difficulties have been encountered with premature termination. Instead, steady-state conditions are typically attained by controlling boundary conditions and executing in the transient mode. With this technique, convergence can be expedited by manually reducing the thermal capacitances. Once a satisfactory steady-state condition has been calculated, the true capacitances are restored before performing transient calculations.

The strip mode is used to extract specific data channels from the output file of an existing calculation. In this mode, the restart/plot file and a file containing the list of desired data channels are executed. The resulting output is a compacted file, containing only pertinent data, that is suitable for driving a separate plotting routine.

**3.1.3.3 Transient Execution Failures.** An extensive data dump is generated when a transient execution failure is encountered. One or more error messages are contained in the dump explaining the nature and cause of the failure. These error messages are usually not as informative as error messages concerning input errors. A typical error message might, for example, indicate a water property failure in cell 12001. The user should understand that this condition, perhaps a pressure above the critical point, is the immediate cause of code failure and not necessarily the root cause of the failure. Scrutinizing the major edit at the failure point should be the first step in identifying the problem.

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a. The user should specify the edit frequency carefully. A huge quantity of output can be generated that may require large amounts of disk storage space.

A common cause of transient execution failure is mis-specification of initial or boundary conditions. If, for example, a loss-of-coolant accident transient is initiated from a calculated steady condition and a failure is encountered shortly after the calculation begins, a frequent cause is an unintended perturbation of the steady conditions by the user. The user should confirm that initial and boundary conditions (and changes in them as the transient is initiated) are appropriate. If boundary and initial conditions appear to be in order, the next step should be to significantly reduce the maximum time step size selected.

**3.1.3.4 Normal Termination of Transient Execution.** The normal termination of a transient calculation may be accomplished one of three ways. First, a normal job termination occurs when the problem time reaches the end time specified on the last time step control card (201-299). Second, a normal job termination occurs when the computer time expended reaches the limit specified by the inputs on the 105 control card. Third, a normal job termination may occur by trip, as specified on the 600 card. Thus, the user has the flexibility of terminating the calculation based on problem time, computer time, or some occurrence in the calculation (e.g., when a pressure limit is exceeded). It is important for the user to ensure a normal termination using one of these methods. Failing to internally (i.e., within RELAP5) stop the calculation before expending all the computer time requested on an external job card will result in an abnormal termination. In that case, some or all of the data generated by the job may be lost.

#### 3.1.4 Code Output

There are two forms of code output for each calculation: printed output and the restart/plot file.

**3.1.4.1 Printed Output.** During execution of the code, a printed output file is generated according to the options selected. A typical output file begins with a simple listing of the input. The listing is followed by input processing information, including an echo of the input requested. This echo represents the actual data accepted by the code for each of the input values. Note that there is a chance of interpretation error (e.g., in the case of replacement cards). When a card number appears more than once in an input deck, only the input contained on the last card entered is used by the code. The presence of a replacement card is noted in the input listing; however, the message appears adjacent to the replacement card, not the original card. Therefore, it is to the user's advantage to use the echoed input, not the listing of the input, as a true indication of the input used.

The printed output file continues with a listing of the initial major edit. This edit is, in turn, followed by the major edits as requested by the user and additional major edits generated by the code. The minor edits, requested by the user on cards 301-399, are interspersed between the major edits (the major edits are printed at intervals such that the minor edits fill a full page). Additionally, warning messages may be printed between the major edits, indicating the nature and times of non-fatal calculational difficulties. Restart edits are annotated with a restart number; the message appears following the major edit data. An annotated sample major edit appears in Figure 3-3.





Figure 3-3. (continued) notes

1. The major edit header region contains information regarding the progress of the calculation. Data described as "total" are from the beginning of the calculation; data described as "edit" are from the previous major edit. In the example shown, the calculation is running at the maximum (or requested) time step size; no time step reductions have occurred. The computer central processing unit time consumed up to this point is displayed. The Courant limit is displayed. The data on the right hand side are used to determine if cumulative mass error is significant. In the example, the ratio of mass error to problem mass is of the magnitude  $10^{-7}$ ; therefore, mass error is insignificant.

2. This region displays the current status of all trips. A value of -1.0 indicates the trip is currently false. Trips shown with positive values are currently true, and the value shown is the time when the trip last turned from false to true.

3. This region displays the current conditions of all hydrodynamic volumes. The data are displayed in four sections (3A, 3B, 3C, and 3D) and the volume identifier is shown at the left margin in each section. The fluid state is displayed in Section 3A. The column titled "pressure" is the total pressure; the partial pressure of steam is shown in the following column. The difference between the first two columns, if any, is the partial pressure of non-condensable gas. The next two columns, titled "voidf" and "voidg" display the liquid and vapor fractions within the volume, respectively. These two columns add to unity. The terms "voidf" and "voidg" are inaccurate since the term "void" is actually only associated with vapor. The next three columns display the temperatures of the liquid and vapor phases and the saturation temperature at the volume pressure. The specific internal energies of the liquid and vapor phases are next displayed. For easy reference, the final column shows the packed word (pvbfe) control flags for the volume.

Section 3B starts with a display of the liquid and vapor phase densities, the density of the fluid mixture, and the boron density in the volume. Next, the volume phase velocities and the volume sound speed are displayed. Note that the phase velocities are based on the volume flow area, which may be different from the junction flow areas. Finally, the mixing cup quality, static quality, and non-condensable quality are displayed. The mixing cup quality assumes any phasic nonequilibrium is removed. A negative mixing cup quality indicates subcooled liquid. Its magnitude is normalized to the latent heat of vaporization.

Section 3C provides volume transport conditions and properties. The column titled "tot. ht." is the total heat transfer rate into the volume fluid from heat structures. The vapor heat is the heat transfer rate from the heat structures to the vapor phase. The difference between the first two columns is the heat addition rate from heat structures to the liquid phase. A positive heat transfer is defined as being from the walls to the fluid. The column titled "vapor gen." displays the total vapor generation rate. This rate is normalized to a unit volume. The total rate is the sum of the vapor generation from interphase mass transfer and from boiling on the wall. The following column, titled "wall-flashing," shows the rate of vapor generation from boiling. The difference between the columns is the

Figure 3-3. (continued) notes

interphase vapor generation rate component. The liquid- and vapor-side heat transfer coefficients are displayed in the following columns. Interphase heat transfer employs the concept of a saturated interface and these coefficients represent the paths from the phases to the interface. For reference, the volume mass flux, phasic Reynolds Numbers, and flow regime are shown in the remaining columns. The flow regime is indicated by an acronym: bby=bubbly, hat=horizontal stratified, anm=annular mist, slg=slug, ian=inverted annular, isl=inverted slug, and ctb=churn turbulent.

The data in Section 3D provide an indication of the causes and model regions limiting calculation progress. The data shown indicate, both on a total basis and for the edit, the volume with the largest mass error and the volume controlling the Courant limit. The columns labeled "reduce-" show the number of occurrences where the volume has resulted in time step reduction. For perspective, the number of occurrences should be compared with the "edit" and "total" number of successful advancements shown in Section 1.

4. Section 4 displays the hydrodynamic state of the junctions. The junction identifier appears in the left hand column of Section 4A followed, for reference, by identifiers of the volumes the junction connects. Next, the phasic velocities and mass flow rates are displayed. For reference, the junction flow area, throat ratio, and junction control flags (packed word fvcahs) are shown. Depending on the junction options selected, the junction area displayed may not be that specified in the model input and used by the code. The true junction area, which may vary in time (e.g., at a valve junction), is the product of the junction area and throat ratio.

The final three columns in Section 4A indicate the current status and history of choking at the junction. In the column titled "last," a value of 0 indicates an unchoked condition and a value of 1 indicates a choked condition on the last time step. In the next two columns, the number of choking occurrences since the last major edit and from the beginning of the calculation are shown. For perspective, the number of occurrences should be compared with the "edit" and "total" number of successful advancements shown in Section 1.

In Section 4B, the junction liquid and vapor fractions are shown (see discussion in note 3 above). The following 7 columns, with titles beginning with "f" present data describing the components of junction friction pressure drop. "fij" represents the interphase drag. "fwalf" and "fwalgj" represent the wall drag components on the liquid and vapor phases. The wall drag is based on flow between the adjacent volume cell centers through the junction. The columns titled "fjunl" and "fjunr" represent the phasic losses from user-input flow loss coefficients. The columns titled "formfj" and "formgj" represent the phasic losses from code-calculated flow losses (such as abrupt area change effects). The last three columns in Section 4B describe the current status and history of the operation of the countercurrent flow limiting model (the displayed information is comparable to that shown for the choking model described above).

Figure 3-3. (continued) notes

1. The major edit header region contains information regarding the progress of the calculation. Data described as "total" are from the beginning of the calculation; data described as "edit" are from the previous major edit. In the example shown, the calculation is running at the maximum (or requested) time step size; no time step reductions have occurred. The computer central processing unit time consumed up to this point is displayed. The Courant limit is displayed. The data on the right hand side are used to determine if cumulative mass error is significant. In the example, the ratio of mass error to problem mass is of the magnitude  $10^{-7}$ ; therefore, mass error is insignificant.

2. This region displays the current status of all trips. A value of -1.0 indicates the trip is currently false. Trips shown with positive values are currently true, and the value shown is the time when the trip last turned from false to true.

3. This region displays the current conditions of all hydrodynamic volumes. The data are displayed in four sections (3A, 3B, 3C, and 3D) and the volume identifier is shown at the left margin in each section. The fluid state is displayed in Section 3A. The column titled "pressure" is the total pressure; the partial pressure of steam is shown in the following column. The difference between the first two columns, if any, is the partial pressure of non-condensable gas. The next two columns, titled "voidf" and "voidg" display the liquid and vapor fractions within the volume, respectively. These two columns add to unity. The terms "voidf" and "voidg" are inaccurate since the term "void" is actually only associated with vapor. The next three columns display the temperatures of the liquid and vapor phases and the saturation temperature at the volume pressure. The specific internal energies of the liquid and vapor phases are next displayed. For easy reference, the final column shows the packed word (pvbfc) control flags for the volume.

Section 3B starts with a display of the liquid and vapor phase densities, the density of the fluid mixture, and the boron density in the volume. Next, the volume phase velocities and the volume sound speed are displayed. Note that the phase velocities are based on the volume flow area, which may be different from the junction flow areas. Finally, the mixing cup quality, static quality, and non-condensable quality are displayed. The mixing cup quality assumes any phase nonequilibrium is removed. A negative mixing cup quality indicates subcooled liquid. Its magnitude is normalized to the latent heat of vaporization.

Section 3C provides volume transport conditions and properties. The column titled "tot. ht. inp" is the total heat transfer rate into the volume fluid from heat structures. The vapor heat input is the heat transfer rate from the heat structures to the vapor phase. The difference between the first two columns is the heat addition rate from heat structures to the liquid phase. By convention, positive heat transfer is defined as being from the walls to the fluid. The column titled "vapor-gen." displays the total vapor generation rate. This rate is normalized to a unit volume basis. The total rate is the sum of the vapor generation from interphase mass transfer and vapor generation from boiling on the wall. The following column, titled "wall-flashing," shows the vapor generation rate from boiling. The difference between the columns is the



Figure 3-3. (continued) notes

interphase vapor generation rate component. The liquid- and vapor-side heat transfer coefficients are displayed in the following columns. Interphase heat transfer employs the concept of a saturated interface and these coefficients represent the paths from the phases to the interface. For reference, the volume mass flux, phasic Reynolds Numbers, and flow regime are shown in the remaining columns. The flow regime is indicated by an acronym: bby=bubbly, hst=horizontal stratified, anm=annular mist, slg=slug, ian=inverted annular, isl=inverted slug, and ctb=churn turbulent.

The data in Section 3D provide an indication of the causes and model regions limiting calculation progress. The data shown indicate, both on a total basis and for the edit, the volume with the largest mass error and the volume controlling the Courant limit. The columns labeled "reduce-" show the number of occurrences where the volume has resulted in time step reduction. For perspective, the number of occurrences should be compared with the "edit" and "total" number of successful advancements shown in Section 1.

4. Section 4 displays the hydrodynamic state of the junctions. The junction identifier appears in the left hand column of Section 4A followed, for reference, by identifiers of the volumes the junction connects. Next, the phasic velocities and mass flow rates are displayed. For reference, the junction flow area, throat ratio, and junction control flags (packed word fvcahs) are shown. Depending on the junction options selected, the junction area displayed may not be that specified in the model input and used by the code. The true junction area, which may vary in time (e.g., at a valve junction), is the product of the junction area and throat ratio.

The final three columns in Section 4A indicate the current status and history of choking at the junction. In the column titled "last," a value of 0 indicates an unchoked condition and a value of 1 indicates a choked condition on the last time step. In the next two columns, the number of choking occurrences since the last major edit and from the beginning of the calculation are shown. For perspective, the number of occurrences should be compared with the "edit" and "total" number of successful advancements shown in Section 1.

In Section 4B, the junction liquid and vapor fractions are shown (see discussion in note 3 above). The following 7 columns, with titles beginning with "f" present data describing the components of junction friction pressure drop. "fij" represents the interphase drag. "fwalfj" and "fwalgj" represent the wall drag components on the liquid and vapor phases. The wall drag is based on flow between the adjacent volume cell centers through the junction. The columns titled "fjunf" and "fjunr" represent the phasic losses from user-input flow loss coefficients. The columns titled "formfj" and "formgj" represent the phasic losses from code-calculated flow losses (such as abrupt area change effects). The last three columns in Section 4B describe the current status and history of the operation of the countercurrent flow limiting model (the displayed information is comparable to that shown for the choking model described above).

**Figure 3-3.** (continued) notes

5. Sections 5A and 5B show the current status of the model heat structures. Section 5A starts with the heat structure geometry number; the hydrodynamic volume connections are shown for the left and right sides for reference. If a boundary volume of 0-000000 is shown, the surface is adiabatic. The following columns show the surface temperatures, heat transfer rates, and heat fluxes. The next column shows the critical heat fluxes. Depending on the current status of the heat structure, actual critical heat flux data may not be printed. Critical heat flux is not calculated (and a 0.00000 is printed) if no boiling is present, such as in single-phase forced convection. If a user-specified critical heat flux multiplier has been used, it appears for reference in the next column. The following column shows the heat transfer mode number; the user is referred to the code manual for the correlation of heat transfer modes and numbers. The next column shows the heat transfer coefficient. This coefficient is consistent with the fluid temperatures, heat structure surface temperature, heat flux, heat transfer rate, and heat transfer area for each surface of the structure. If an internal heat source is used, such as for a fuel rod, its magnitude is displayed in the following column. The column titled "conv+rad-source" represents the total heat balance on the structure. The final column shows the volume average temperature of the heat structure. Section 5B shows the current node temperatures for each structure. The first temperature is for the left surface; the last temperature is for the right surface.

6. Section 6 shows the current values of all control variables. The control variable number, its descriptive name, its type, and the current value are displayed.

7. If the major edit is also a restart edit, then Section 7 is printed. The restart number shown here is the one required on the 103 control card for a restart run. The block number is not used.



**3.1.4.2 The Restart/Plot File.** The restart/plot file contains virtually all calculation parameters (pressures, temperatures, void fractions, flow rates, etc.) for the entire transient calculation.

A common misconception is that a parameter needs to be specified using a minor edit request in order to be available in the output when the calculation is complete. A minor edit request affects only the printed output. It is not necessary to specify all the parameters needed for output in advance; this determination may be made after the calculation has been completed. The output file may be accessed repeatedly as new data needs arise. However, during a calculation, data are written to the restart/plot file only at the minor edit frequency. Once a calculation has been performed, it is not possible to recover the data between the data points written to the file. Therefore, it is important to select a minor edit frequency that will provide plot points at an interval appropriate for the problem being solved. In practice, the minor edit (and plot point) frequency should be changed during as the problem proceeds from one phase to the next. Frequent points should be selected during problem phases where rapid changes in parameters are expected. For economy, less frequent points should be selected during phases where quiescent conditions are expected.

Calculations typically are accomplished using multiple restarts. For example, a new problem is run from 0 to 10 seconds. This early portion is analyzed and rerun from time zero as errors are corrected. When a successful calculation to 10 seconds has been made, a restart run is made (e.g., from 10 to 30 seconds), and so on. RELAP5 provides the flexibility to change virtually any feature of the model at any restart point. When model changes are incorporated on restart, the restart/plot file reflects those changes only after the point in the calculation where they were implemented. In the above example, if an injection system is added to the model at 10 seconds, then data for the added components exists only for times after 10 seconds. Model additions, deletions, and changes are permanently implemented. If a model change is made at 10 seconds, the revised model remains in effect unless further modifications are made at subsequent restart points.

When a calculation has been completed, the restart/plot file becomes a valuable record of the calculation. If lost, replacing it would require reperforming the calculation, generally at considerable expense. At any later date, the file may be accessed and previously unaccessed data may be obtained as needed to extend analysis. Therefore, it is recommended that the restart/plot files of important calculations be protected securely and permanently.

## 3.2 Calculational Node And Mesh Sizes

This section provides guidance for selecting the nodal sizes of hydrodynamic cells and the mesh sizes of heat structures.

For economic reasons, the numbers of hydrodynamic cells and heat structure mesh points in general should be minimized. The computer run time needed to execute a problem simulation is determined almost completely by the number of hydrodynamic cells in the model. The number of heat structures generally increases in tandem with the number of cells. Therefore, a major

economic benefit is gained by limiting the number of hydrodynamic cells in a model. Some additional economic benefit may be obtained by minimizing the number of mesh points within the heat structures. Limiting the number of other model features (such as trips and control variables) provides only minimal economic benefits.

There is an additional motivation for employing the largest calculational cells possible. When small cells are used, the time step size is reduced as a result of the material Courant limit. The Courant limit, discussed in Section 3.1, limits the calculational time step based on the ratio of cell length to fluid velocity.

The process of minimizing model size must, however, always consider the phenomena to be modeled; minimizing must not proceed past the point where important phenomena are excluded from the simulation. This consideration is complicated, however, because the importance of phenomena varies from one region of the model to another and is strongly affected by the transient to be simulated. For example, the important model regions and simulation phenomena for small and large break loss-of-coolant accidents are dramatically different; therefore, appropriate modeling for these two sequences varies dramatically.

In summary, the modeler should select the minimum number of hydrodynamic cells and heat structure mesh points needed to calculate the important phenomena for the simulated transient. This guidance suggests that a general model (i.e., one that is to be used to simulate many different types of transients) should contain sufficient noding detail for all phenomena anticipated. If the important phenomena are uncertain, a detailed noding scheme should be employed. Conversely, if the important phenomena are well known, nodalization of the non-critical model regions may be simplified. If sufficient time and funds are available, it is recommended that a general model of a reactor system be assembled first. Analysis using the general model will then provide the information needed to determine what model simplifications are appropriate. The following sections provide additional guidance concerning hydrodynamic cell and heat structure sizing. General suggestions for appropriate noding may be inferred from the example problem applications in Section 5.

### 3.2.1 Hydrodynamic Cell Size

As discussed above, large hydrodynamic cell sizes should be used for economic reasons. However, in each region of the model, the detail of the calculational cells must be sufficient to allow the simulation of important regional thermal-hydraulic phenomena. As a starting point, cell lengths of 1 to 3 m (3 to 10 ft) are recommended in phenomena-dominating regions (e.g., reactor vessel, pressurizer, and steam generator) of a light water reactor model. Cells of much longer lengths are appropriate in less important regions of the model (e.g., the feedwater train and steam lines). Example models, with nodalization schemes that have evolved over years of experience, are provided in Section 5. The cell sizes presented in these applications may be taken as guideline recommendations for modeling light water reactors. For totally new applications or where the calculation results may be particularly sensitive to the model discretization, a convergence study is recommended to ensure that a proposed nodal layout is adequate.

Good modeling practice includes blending the transition from regions of small cells to regions of large cells. For this blending, it is recommended that the volumes of adjacent cells not differ by more than an order of magnitude.

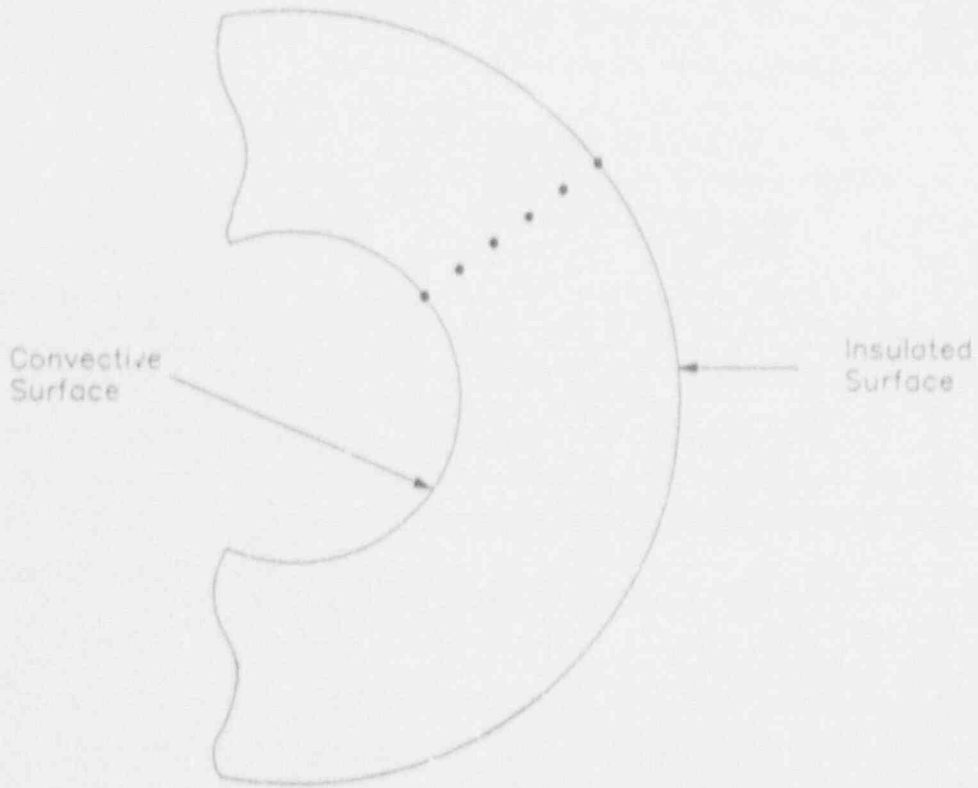
Other considerations affecting cell size selection are the locations of natural boundaries, flow connections, and instruments within the prototype fluid system. Good modeling practice includes placing junctions at natural fluid system boundaries and at flow loss features (such as support plates, grid spacers, bends, and orifices). Using this practice, the flow loss is placed at the proper location with respect to the fluid volumes. For similar reasons, the placement of junctions at flow connection points is a good practice. Cell size selection should also consider placing model features at prototypical instrument locations (e.g., placing a cell center at the location of a pressure tap or a junction at the location of a flow meter). This practice facilitates the use of the code output because the calculated and measured data are directly comparable without further effort.

### 3.2.2 Heat Structure Mesh Size

As stated above, the computer run time of a model may be improved if the number of heat structure nodes are limited. The minimization process involves a trade-off between the number of nodes and the calculation error. The fewest number of nodes, consistent with acceptable calculational error, should be used.

To demonstrate this trade-off, consider the simple cylindrical heat structure portrayed in Figure 3-4. The inner surface includes a convective boundary condition of fluid, the outer surface is insulated. The code-calculated heat transfer to the fluid is an approximation based on a finite-difference conduction solution within the heat structure and an assumed heat transfer coefficient on the inner surface. The heat transfer coefficient is based on the calculated flow regime and may involve considerable uncertainty (perhaps 50%). The question to answer is this: "How many heat structure nodes are needed so that the conduction solution error is acceptably small in the context of the overall uncertainty?" The error in the conduction solution will be a function of the speed and magnitude of the thermal transient. Rapid transients involving large temperature changes will result in the largest errors. The conduction solution error may therefore be bounded by evaluating the effects of an instantaneous change in the inside surface temperature by the largest anticipated temperature change. This evaluation may be facilitated by using a simple RELAP5 model of a representative heat structure and performing a noding sensitivity study.

In practice, the effort required to perform the above trade-off is justified only when the temperature solution within a heat structure is of particular significance to the problem. Instead, the number of heat structure nodes is typically selected by convention (some of which were developed by undocumented convergence studies such as described above). These conventions prescribe the use of 2 to 12 nodes. Recommended numbers of nodes include 2 for steam generator tubes, 4 for passive heat structures such as pipe walls, and 12 for fuel rods. For a new application, it is recommended that 6 nodes be used as a starting point for analysis. RELAP5 requires that a node be placed at the interface between two heat structure compositions (such as between a stainless steel clad and carbon steel pipe). Within each composition, nodes are



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Figure 3-4. Heat structure noding.

typically distributed at even intervals with a higher density of nodes used within thermally thick regions or where needed for resolution of heat source distribution within the thickness of the composition.

A special recommendation is made for the gas gap region within a fuel rod. To avoid calculational difficulties resulting from the very low gas gap thermal capacity, it is recommended that no heat structure nodes be placed within the gap region (i.e., between the node on the outer surface of the fuel pellet and the inner surface of the clad).

The user should avoid the temptation to economize by reducing the number of heat structures. Reducing heat structures may lead to significant misrepresentations in the computer model. Furthermore, if the user develops the hydrodynamic portions of a model first, the heat structure models may be developed only as an afterthought. With this process, the heat structures involving the plant energy balance (e.g., fuel rods and steam generator tubes) are included in the model; however, passive heat structures (e.g., piping walls) often are neglected. Ignoring passive heat structures is a common modeling error. Their metal heat capacity is a large fraction of the fluid heat capacity in a plant. It is highly recommended that the hydrodynamic and heat structure input associated with each calculational cell be developed at the same time. In this way, the importance of heat structures to the overall problem may be considered concurrently with the hydrodynamics, a much more satisfactory model development approach.

### 3.3 General Option Selection

Guidelines for the selection of options common to all components are presented in this section. Guidelines for option selection applicable to a specific component (e.g., valves or pumps) appear in Section 4. The following subsections present general guidelines for selecting volume options, junction options, initial conditions, and boundary conditions.

#### 3.3.1 Volume-Related Options

The volume-related options are selected by the volume control flags that are required input for each hydrodynamic volume. The volume control flags are input as a packed word of the format "pvbfe." The default options, obtained by entering 00000, are generally recommended for use.

The p flag specifies whether the water packing scheme is operative. The p = 0 option indicates water packing is to be used, and p = 1 indicates it is not to be used. This is a new option in RELAP5/MOD3; previously, the user did not have the option of deactivating the water packing scheme. It is recommended that the p = 0 option generally be used and the p = 1 option be reserved for situations where calculational difficulties are caused by repeated water packing occurrences. For TMDPVOL, SEPARATR, JETMIXER, TURBINE, PUMP, and ACCUM components, the p flag is not used and 0 should be entered.

The v flag specifies whether the vertical stratification model is to be used. The v = 0 option indicates the vertical stratification model is to be used, and v = 1 indicates it is not to be used. This is another new option in RELAP5/MOD3; previously, the user did not have the option of deactivating the vertical stratification model. It is recommended that the v = 0 option

generally be used. The  $v = 1$  option is reserved for situations where the calculated vertical stratification behavior is not desired. For TMDPVOL, SEPARATR, JETMIXER, ECCMIX, TURBINE, PUMP, and ACCUM components, the  $v$  flag is not used and 0 should be entered.

The  $b$  flag specifies the interphase friction model to be used. The  $b = 0$  option indicates that the normal pipe interphase friction model is to be used. The  $b = 1$  option indicates that the rod bundle interphase friction model is to be used. This is a third new option in RELAP5/MOD3; previously, the user did not have a choice of interphase friction models. The  $b = 0$  option is generally recommended. For model regions with bundle geometries, such as steam generator secondary boiler regions and reactor core regions, the  $b = 1$  option is recommended. There has been little user experience with the new bundle interphase friction model. For SEPARATR, JETMIXER, ECCMIX, TURBINE, PUMP, and ACCUM components, the  $b$  flag is not used and 0 should be entered.

The  $f$  flag indicates if wall friction is to be calculated. The  $f = 0$  option specifies that wall friction is to be calculated, and the  $f = 1$  flag indicates wall friction is not to be calculated. The  $f = 0$  option is generally recommended. The  $f = 1$  option is reserved for special situations where wall friction is undesirable. This situation might arise when a simplified model is constructed of a complex fluid region. In such situations, the input cell length (or that implied from volume and area) may be much longer than is prototypical. The  $f = 1$  option could be used in this case to eliminate the excessive wall friction resulting from the long apparent cell length. For SEPARATR and PUMP components, the  $f$  flag is automatically set to 1, regardless of the value set by the user.

The  $e$  flag indicates whether phasic nonequilibrium or equilibrium options are to be used. In this terminology, "nonequilibrium" implies that the liquid and vapor phases may be at different temperatures. Conversely, "equilibrium" implies that the phases are constrained to be at the same temperature. The  $e = 0$  flag indicates nonequilibrium assumptions are to be used;  $e = 1$  indicates equilibrium assumptions are to be used. The  $e = 0$  option is generally recommended. The  $e = 1$  option is reserved for special situations where the nonequilibrium assumption causes difficulty in obtaining a reasonable solution because of insufficient thermal mixing between the phases. An example of the equilibrium option aiding a simulation is the downcomer of a once-through steam generator. Insufficient interphase condensation may prevent flow of sufficient steam through the aspirator; changing to the equilibrium option may enhance the condensation and improve the aspirator flow. Another example is the upper pressurizer dome region when spray is operating and the pressurizer level is high. In this situation, insufficient interphase condensation may be calculated and changing to the equilibrium option may improve the simulation. For ACCUM components, the  $e$  flag must be set to 0.

### 3.3.2 Junction-Related Options

The junction-related options are selected by the junction control flags that are required input for all junctions except time-dependent junctions. The junction control flags are input as a packed word of the format "fvcahs." The default options, obtained by entering 000000, are generally recommended for use.



The *f* flag specifies whether the countercurrent flow limiting (CCFL) model is operative. The *f* = 0 option indicates the CCFL model is not to be used; *f* = 1 indicates it is to be used. This is a fourth new option in RELAP5/MOD3. Previously, a CCFL model was not available and little user experience exists. It is recommended that the *f* = 0 option be generally used and the *f* = 1 option be reserved for situations where CCFL phenomena are expected. For junctions associated with SEPARATR, JETMIXER, ECCMIX, TURBINE, and ACCUM components, the *f* flag is not used and 0 should be input.

The *v* flag indicates the operative horizontal stratification option. This flag allows the user to specify a junction at a pipe centerline (the default and generally recommended option), or on the top or bottom of a pipe. The *v* = 0 flag indicates a junction at the pipe centerline. The *v* = 1 flag indicates an "upward oriented" junction (i.e., a junction on the top of the "from" volume), and the *v* = 2 flag indicates a "downward oriented" junction (i.e., on the bottom of the "from" volume). The *v* = 3 option permits the user to deactivate all horizontal stratification junction logic. Whenever a volume is in the horizontal stratified flow regime, the *v* = 2 and *v* = 3 options allow the adjacent junctions to pass only steam from an upward oriented junction and only liquid from a downward oriented junction.

The *c* flag indicates whether the choking (critical flow) model is applied at the junction. The *c* = 0 flag indicates choking is active; the *c* = 1 flag indicates it is not active. It is recommended that the *c* = 0 flag generally be used.

The *a* flag indicates the operative area change option. The *a* = 0 flag indicates the smooth area change model is to be used; *a* = 1 indicates the abrupt area change model is to be used. For each junction, the user should consider the geometry of the fluid region to be modeled. In the absence of sharp edged area changes, it is generally recommended that the *a* = 0 option be used. For junctions involving a sharp edge area change the *a* = 1 option is recommended. For motor or servo valve components, either the *a* = 0 or *a* = 1 option may be used. However, if the *a* = 0 option is used, a valve  $C_v$  table must be input; if the table is not input, the *a* = 1 option must be used. For all other types of VALVE components, the *a* = 1 option must be used. The abrupt area change model determines an appropriate junction flow loss based on the flow areas of the junction and adjacent volumes and is suitable for modeling geometries such as pipe-to-plenum, plenum-to-pipe, and orifices. The abrupt area change flow loss is calculated internally by the code and is additive to any user-input flow loss for the junction. This additive property allows the user to combine the code-calculated area change loss with other losses, such as bend losses, at any junction.

The *h* flag indicates the phasic velocity assumption to be used at a junction. The *h* = 0 flag (the recommended option) specifies a nonhomogeneous assumption. With this option, the two-velocity momentum equations are solved and different vapor and liquid phase velocities are calculated. The *h* = 2 flag indicates a homogeneous assumption; the vapor and liquid phase velocities are constrained to be the same.

The *s* flag is used to implement the crossflow model. For each hydrodynamic cell, the main flow is assumed to enter at the inlet face and exit at the outlet face. Junctions on these faces are termed "normal" junctions. A "crossflow" junction is one connected directly at the cell center, not at the cell faces. The *s* = 0 flag indicates a normal junction and this is generally recommended.

For situations where it is desired to connect a junction at the cell center rather than cell face, the crossflow option is implemented by using an  $s = 1$  flag (if the "to" cell is a crossflow volume), an  $s = 2$  flag (if the "from" cell is a crossflow volume), or an  $s = 3$  flag (if both "to" and "from" cells are crossflow volumes). The crossflow option permits the user to simulate multidimensional flow geometries. The user should be aware, however, that a crossflow-linked model does not provide a true three-dimensional modeling capability because the momentum flux term is ignored for crossflow junctions. Therefore, it is recommended that the crossflow junction be avoided in locations where the transverse (crossflow junction) velocity is comparable to or greater than the longitudinal (normal junction) velocities. A crossflow option may not be specified for junctions associated with PIPE, JETMIXER, VALVE, and PUMP components. For ACCUM components, the  $s = 2$  and  $s = 3$  options are not allowed. Specific examples of crossflow junction applications are presented in Section 3.4.

### 3.3.3 Initial Condition Options

The user is required to specify initial conditions for hydrodynamic volume fluid states, hydrodynamic junction flows, heat structure nodal temperatures, and control variable states. In addition, the user has the option to specify the initial status of trips. Guidelines for each of these specifications are discussed separately in the following sections.

The user should carefully consider whether a large effort is needed to specify exact initial conditions for hydrodynamic features. In most cases, this effort is not required and can prove counterproductive in some cases. When building a new model, it is suggested that only very crude initial conditions be specified and the code be used to calculate the steady initial conditions needed as a starting point for transient calculations. For example, all initial fluid temperatures might be set to the cold leg temperature, all initial pressures set to the cold leg pressure, all initial velocities set to zero, and all heat structures and control variables allowed to initialize themselves. The model is then brought up to the desired steady conditions by gradually introducing the fluid flow and heat addition boundary conditions. This simple initialization process is much more economic than attempting to specify exact initial conditions for each model feature.

**3.3.3.1 Volume Fluid State Initialization.** The initial hydrodynamic volume fluid state is specified using the fluid state control word. This is a packed word with format "cbt." The c option specifies the fluid, the b option specifies whether boron is present, and the t option specifies the manner in which the two to five remaining input words are interpreted by the code.

It is recommended that the fluid be specified for each fluid system using either the default assumption (steam/water) or the 120-129 series of fluid system control cards (see Section 4.2) rather than using the c option for each cell individually. Therefore, it is generally recommended that either  $c = 0$  be employed or, equivalently, the c digit omitted.

Options using  $t = 0$  through  $t = 3$  specify a single-component fluid (as indicated by the c option, the fluid system cards, or by default), while options 4 through 6 specify a two-component condition (steam/water and non-condensable gas). Using options 0 and 6, considerable effort is needed to develop the input needed. It is suggested that the user avoid these options when possible. For PWR and BWR applications, options 2 (pressure and quality in equilibrium condition) and 3 (pressure and temperature in equilibrium condition) facilitate fluid state

specification in all regions of the reactor coolant system. Option 2 is recommended for steam regions (e.g., steam lines and steam domes) and two-phase regions (e.g., pressurizer level interface, boilers, and BWR cores). Option 3 is recommended for subcooled liquid regions (e.g., cold legs, hot legs, and PWR cores).

To include either boron or non-condensable gas capability, it is not necessary to identify the capability in every cell of the fluid system (by specifying  $b = 1$  for boron or  $t = 4, 5,$  or  $6$  for non-condensable gas). Boron concentrations and non-condensable gas qualities only need to be specified in cells where they are initially nonzero. If present in any cell of a fluid system, boron and non-condensable gas migration is automatically tracked by the code throughout all cells of the system.

**3.3.3.2 Junction Flow Initialization.** The initial hydrodynamic junction flow condition is indicated by the control word ( $0 =$  velocities specified and  $1 =$  mass flow rates specified). Using either option, velocities or mass flow rates for both the liquid and vapor phase are input. As indicated in Volume 2 (Carlson et al., 1990a), the user must also input a zero interface velocity; this input velocity is not currently used by the code. The choice of entering velocities or mass flow rates is usually determined by convenience and by availability of information.

A common user error is to mis-specify a junction initial condition, which causes an unintended step change in the code calculation. Often, this error results in a water property failure shortly after the calculation is initiated. To avoid difficulty, the user should ensure that each junction initial condition specified is consistent with the fluid state of the upstream cell and with the initial conditions of the upstream junctions.

**3.3.3.3 Heat Structure Initialization.** The initial heat structure state is specified by the steady-state initialization flag (word 4 on the first input card of each heat structure). If a 0 flag is used, the initial heat structure node temperatures are set to those input by the user. If a 1 flag is used, the initial heat structure node temperatures are calculated by the code based on steady heat transfer considerations and the initial fluid conditions of the adjacent hydrodynamic cells. Note that the user must input the required number of initial temperatures, even though they are not used when the 1 flag is used. In general, for new models it is recommended that the 1 flag be used. The choice of the heat structure initialization flag is particularly important if heat structures are reinput on restart during the course of a transient calculation. The user should be aware that in this situation, the 0 flag should be used to specify the node temperatures. A common error is to have the 1 flag set, resulting in a step change in heat structure temperatures at the restart time.

**3.3.3.4 Control Variable Initialization.** Control variable initialization is determined by the initial value flag (word 5 on the first card of each control variable input). If the 0 flag is used, the initial value specified in word 4 is used as the initial condition. If the 1 flag is used, the initial condition is computed based on the control variable format and the initial values of any referenced parameters.

The user is cautioned that control variable references to thermohydraulic parameters are always evaluated in International System of Units (SI) units, even when British units are specified using the problem control option. Another caution regards the sequence used to evaluate control variables. Control variables are evaluated last (i.e., following hydrodynamics, heat structures, and

trips) and in numerical order. It is not possible to recommend the general use of a 0 or 1 control variable initialization flag. The user should determine which option is most appropriate for each control variable.

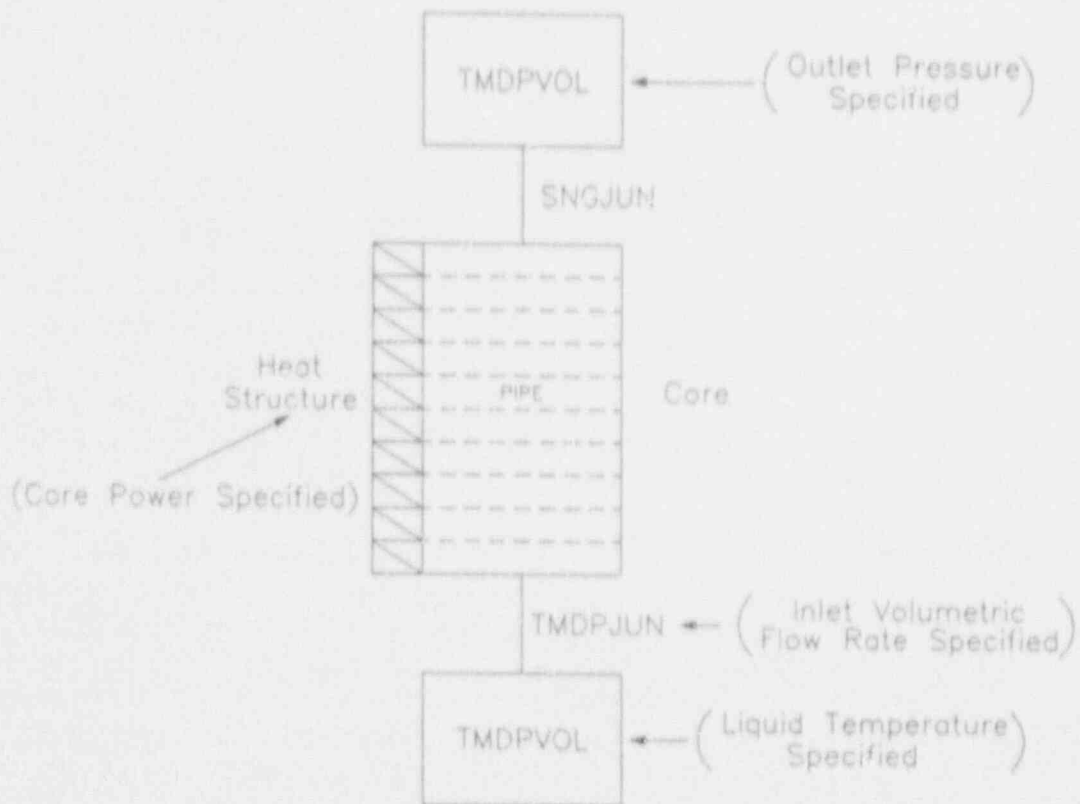
**3.3.3.5 Trip Initialization.** The capability, but not the requirement, to specify an initial trip status is available for both variable and logical trips. This specification is made using the TIMEOF quantity (word 8 on variable trip statements and word 5 on logical trip statements). If a false initial condition is desired, -1 is entered. If a true initial condition is desired, a non-negative floating point time is entered. For most new and restart problems, it is recommended that the true initial condition be attained by entering 0. For restart problems, a positive TIMEOF quantity provides a mechanism for specifying a "last turned true" time before the restart time. This capability allows the trip history to be retained when a trip is reinput on restart.

### 3.3.4 Boundary Condition Options

It is essential that appropriate boundaries for a model be determined early in the modeling process. Proceeding without this consideration is a significant modeling error that may lead to incorrect analysis conclusions. The appropriate model boundaries are those for which all external influences may be condensed into a known set of conditions at the boundary locations. This consideration often involves engineering judgments. A large boundary condition uncertainty is acceptable if its effect on the modeled processes is small; however, a small boundary condition uncertainty is unacceptable if its effect on the modeled processes is large.

Depending on boundary condition assumptions, models are often categorized as "separate effects" or "systems effects" models. The difference is the extent of model reliance on boundary assumptions. An example of boundary conditions for a separate effects model is shown in Figure 3-5. The model represents a PWR core region and is intended to investigate reflood phenomena. The boundary conditions specified include the inlet liquid temperature, the inlet coolant velocity, the outlet pressure, and the core power. In combination, these assumptions are highly uncertain because they likely either assume constant pressure, velocity, and temperature, or assume knowledge of how these parameters vary with core response. Despite the uncertainties, the separate effects model is valuable because it facilitates study of localized model performance and nodalization sensitivities.

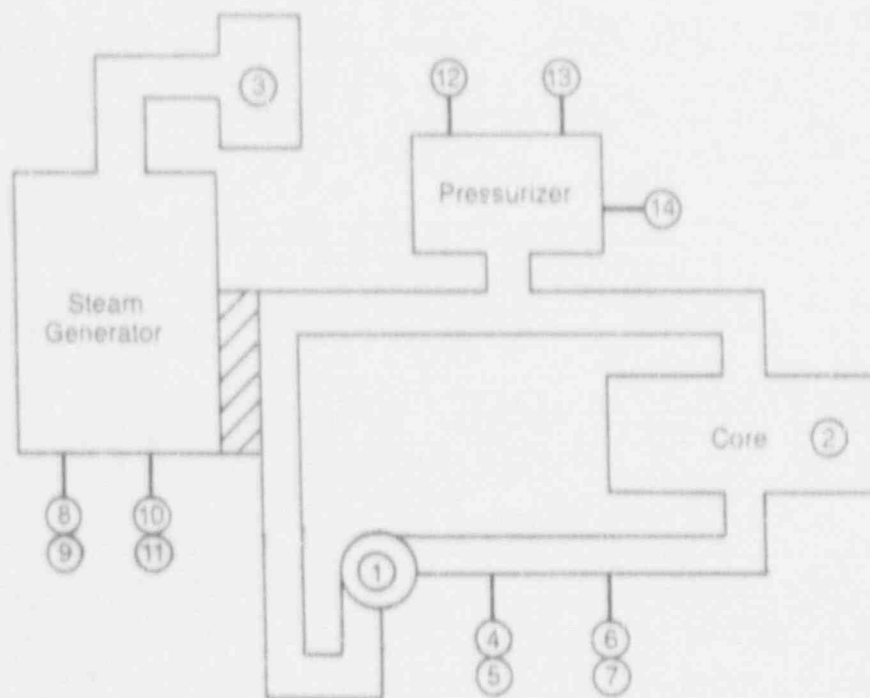
The simplified PWR diagram shown in Figure 3-6 provides an example of system model boundary conditions. Fluid pressure boundary conditions are applied for the outlets of the pressurizer, steam generator safety valves, and power-operated relief valves (PORVs), and for the turbine. Fluid temperature boundary conditions are applied for the safety injection, makeup, and main and auxiliary feedwater systems. Fluid flow boundary conditions are applied for the safety injection (high-pressure and low-pressure injection), makeup, main and auxiliary feedwater systems, and for the main coolant system recirculation (by way of pump speed control). Heat source boundary conditions are applied for the core power and pressurizer heaters. In addition, adiabatic surface boundary conditions are typically assumed on the exterior of insulated piping. Compared to the separate effects model described above, the systems effects model boundary condition assumptions clearly are more certain because they include measured or atmospheric pressures, measured temperatures, and measured flow rates.



HD40-COF-0291-02

Figure 3-5. Example of separate effects core model.





Boundary condition summary

No.	Type	Comment
1	Flow	Pump speed determines coolant flow
2	Power	Core power from table
3	Pressure	Turbine pressure
4	Flow	HPI/LPI flow vs. cold leg pressure
5	Temperature	HPI/LPI fluid temperature
6	Flow	Makeup flow vs. pressurizer level
7	Temperature	Makeup fluid temperature
8	Flow	Feedwater flow
9	Temperature	Feedwater temperature
10	Flow	Auxiliary feedwater flow
11	Temperature	Auxiliary feedwater temperature
12	Pressure	Atmospheric for safety discharge
13	Pressure	Relief tank for PORV discharge
14	Power	Pressurizer heater power

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Figure 3-6. Simplified diagram of PWR system model boundary conditions.



Discussions regarding the application of fluid state, fluid flow, and heat transfer boundary conditions are presented below.

**3.3.4.1 Fluid State Boundary Conditions.** A fluid state boundary condition (pressure, temperature, quality, or void fraction) is implemented with a time-dependent volume (TMDPVOL) component. This name is inaccurate; originally, fluid conditions could be specified only as a function of problem time. Current TMDPVOL capabilities include varying the fluid condition in any manner and as a function of any problem variable the user desires. Detailed user guidelines for time-dependent volumes are found in Section 4.6. The remainder of this section regards their use for specifying boundary conditions.

The TMDPVOL provides the user with a mechanism for absolutely defining the fluid condition at a point in the model. The user should consider that a TMDPVOL acts as an infinite fluid source or sink. Its conditions remain unchanged (or vary) as requested, but are invariant with inflow or outflow. In nuclear safety system model applications, the need to define the fluid state is typically encountered in two situations: defining back pressures and defining liquid temperatures.

Examples where back pressures are required include the discharges of valves and breaks, and the turbine header. Valves that discharge to the atmosphere typically are modeled using a constant pressure TMDPVOL at the discharge. In addition, for valves that discharge into a complex piping network, the user has the option of (a) modeling the network to a point where the pressure is well known, or (b) estimating the pressure drop through the network and adjusting the TMDPVOL pressure at the valve accordingly.

Examples where liquid temperatures are required include the sources for main and auxiliary feedwater, safety injection, and makeup. Typically, these applications assume a constant liquid temperature. However, the capability exists, if the user desires, to include other effects such as a change in liquid temperature as a result of sweeping warm liquid out of a line.

**3.3.4.2 Fluid Flow Boundary Conditions.** A fluid flow boundary condition (velocity or mass flow rate) is implemented with a time-dependent junction (TMDPJUN) component. This name is also inaccurate because originally, fluid flow could be specified only as a function of problem time. Current TMDPJUN capabilities include varying the flow condition in any manner and as a function of any problem variable the user desires. Detailed user guidelines for time-dependent junctions are found in Section 4.6. The remainder of this section regards their use for specifying boundary conditions.

The TMDPJUN provides the user with a mechanism for absolutely defining an inflow or outflow at any location in the model. The TMDPJUN specification must consider the conditions in the upstream volume. If a constant upstream fluid state is specified with a TMDPVOL, then the TMDPJUN may use either a velocity or an equivalent mass flow boundary condition. However, care should be exercised if the upstream fluid state may change during the course of a problem. Consider a problem where the upstream TMDPVOL conditions change during the course of a transient. In this situation, the TMDPJUN will continue to supply the user-requested volumetric or mass flow condition, depending on whether the velocity or mass flow option is used.

Note, however, in this situation that the nonrequested rate (volume or mass) will change as a result of the change in the upstream condition.

In nuclear safety system model applications, the need to define a flow condition is encountered at injection sites for feedwater, auxiliary feedwater, safety injection, and makeup. In these situations, it is recommended that the injection fluid temperature be defined using a TMDPVOL component and that a TMDPJUN component draws fluid from the TMDPVOL and injects it into the reactor coolant system. For situations where the injection flow is known as a function of the reactor coolant system pressure (such as for safety injection), delivery curves can be incorporated into the TMDPJUN. This is accomplished by specifying the TMDPJUN flow as a function of the adjacent reactor coolant system hydrodynamic equilibrium pressure.

The use of TMDPJUN components for specifying outflow from the reactor coolant system or internal flows within the reactor coolant system is not recommended because the upstream fluid conditions may change rapidly, causing solution difficulties. An example of this situation is the letdown system of a PWR. Assume a TMDPJUN is used to model the letdown as a constant mass flow from the cold leg to a TMDPVOL. With this model, the same mass flow rate of liquid will be removed from the reactor coolant system, regardless of the fluid condition within the cold leg. If the model is used in a transient where cold leg voids appear, then the code will encounter difficulties in attempting to continue removing only liquid from a cell where both liquid and vapor are found. The difficulties can be circumvented to some extent by specifying a volumetric rather than mass flow condition. With this method, however, the user must understand that the volumetric flow will continue, even if two-phase fluid or single-phase steam is present in the cold leg. A preferable method for modeling the letdown is to use a VALVE component connected to a TMDPVOL. The VALVE is sized to pass the desired normal flow and the pressure in the TMDPVOL is specified to best simulate the letdown flow response during transients.

**3.3.4.3 Heat Structure Boundary Conditions.** Several boundary conditions may be specified using heat structures. Heat sources may be specified within a heat structure. These sources may be determined either by evaluating a general table [such as one specifying the American Nuclear Society (ANS) standard decay heat following a reactor trip] or by the output of the reactor kinetics model. A variety of options are available for applying external boundary conditions on the surfaces of heat structures. The most common heat structure surface external boundary condition is adiabatic. In general, the adiabatic boundary condition is satisfactory for the external surfaces of insulated reactor coolant system pipes. However, for particularly long transients, heat loss to the environment can become an important effect. The code user should ensure that this is not the case prior to generally applying the adiabatic surface option. Other heat structure surface boundary options allow the user to specify surface temperature, heat transfer coefficient, or heat flux as an external boundary assumption. Further discussion of heat structure boundary conditions appears in Section 4.7.

## 3.4 Special Model Applications

This section describes several special application techniques.

### 3.4.1 Break Modeling

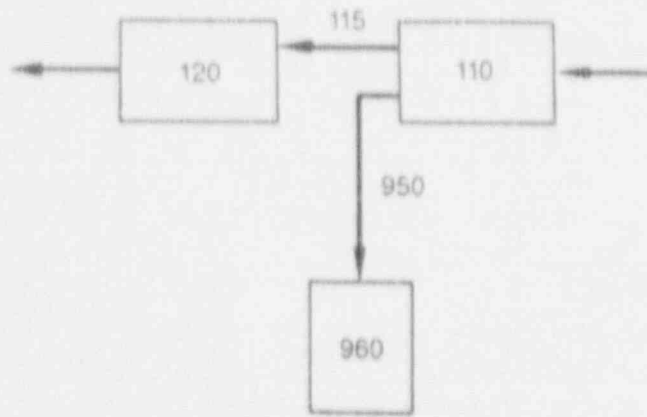
A common code application is simulating a loss-of-coolant accident (LOCA) involving the full or partial rupture of a coolant pipe within an air-filled containment. These applications may involve experimental facility or full-scale plant LOCA simulations.

The need to adequately measure the break flow in an experimental facility usually dictates a complex experimental break geometry to provide clearance for instrumentation. The experimental facility break design often involves a side pipe leading from the broken pipe to a break orifice and valve. This complex design is best modeled in detail (i.e., the geometry upstream and downstream of the break should be modeled directly). Courant limiting considerations will be important in this application because the fluid velocities in the pipe leading to the break will be large. In most analyses of experimental facility LOCAs, benchmarking the break flow path has been necessary to compensate for uncertainties in the break path resistance and the code break flow models. The benchmarking process consists of using experimental data that characterize the break resistance to adjust the model flow losses for an adequate comparison between measured and calculated break flow. The adjustment is typically accomplished by adjusting the discharge coefficients on the break junction.

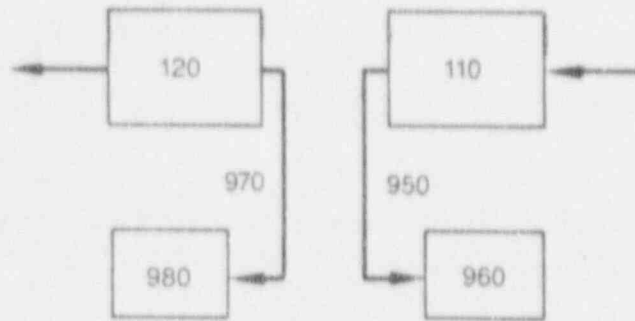
For full-scale plant applications, the break modeling process typically is more straightforward because the break geometry is simpler. Common LOCA applications for full-scale plants include the opening of circular breaks on the top, side, or bottom of a coolant pipe and the double-ended break of a coolant pipe. For full-scale plants, breaks typically are assumed to open instantly. Figure 3-7 shows a recommended nodalization for modeling small and double-ended breaks in a coolant pipe. In both applications, the broken pipe is simulated with volumes 110 and 120.

The small communicative break is simulated by adding single junction 950 and TMDPVOL 960 to the existing hot leg pipe model. The term "communicative" implies a portion of the normal flow through the pipe continues after the break is opened. Note that the break components may be installed on restart, at the time of break opening, by including components 950 and 960 in the input stream. Break junction 950 should employ the abrupt area change option, simulating the combined flow losses associated with the sharp-edged area reduction from the pipe to the break plane and the sharp-edged expansion from the break plane to the containment. Junction 950 should employ the choking option and be initialized at a zero flow condition. The junction control flags provide the capability to locate the break on the top, side, or bottom of the pipe.

TMDPVOL 960 simulates the containment into which the break discharges; this implies the containment state is a boundary condition in the calculation. Frequently, a constant-pressure containment assumption is used. If the containment pressure response is known (e.g., as a function of the integrated break flow), then that response may be included in the simulation. For the double-ended break the nodalization includes two break junctions and two TMDPVOLs, as shown in Figure 3-7. Note that two TMDPVOLs are needed because no more than one junction may be attached to a TMDPVOL. As for the small break, the break junctions should employ the abrupt area change and choking options. Care should be used when specifying the initial break



Communicative break



Double-ended break

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Figure 3-7. Coolant system break modeling.

conditions. In the example shown, the initial mass flow rate for junction 950 should be positive at the same rate as at the inlet to volume 110; the initial mass flow for junction 970 should be negative and of the same magnitude.

In the above examples, the breaks also could have been implemented by including trip valve components at the break junctions in the original model rather than by adding them on restart. The valves would then be tripped open at the time of the break. Using this technique, the breaks may be opened at any time, not just at a restart point.

The containment condition specification is more important in some applications than in others. For small break applications, the primary coolant system depressurization typically is small, the pressure drop across the break remains large, and the break flow remains both choked and positive (into the containment). The containment conditions specified in this situation are not particularly significant to the simulation. The problem is only moderately sensitive to the containment pressure and is insensitive to its gas species. However, for large breaks, transitions between choked- and friction-dominated flow, and intermittent reverse flow from the containment are likely. In this case, it is important to adequately specify the containment conditions.

For some problems where the response of the containment is particularly important, it may be possible for an approximation of the containment behavior to be included as a part of the model. This could be accomplished by modeling the containment and the actual containment mass and heat balances. The code has not been extensively applied in this manner, however.

As a final note, the analyst should appreciate that critical break flow simulation represents an area of significant uncertainty. For some problems, this uncertainty may be a controlling factor for the outcome of the simulation. It is therefore recommended that care be taken to independently check code-calculated break flow results either against experimental data in similar geometries or against standard critical flow correlations.

A recommended procedure for correctly specifying the break area and discharge coefficient is linked to the break scenario, the break plane geometry, and whether any data exists for that geometry. Assuming a discharge coefficient of 1.0 is valid, the following generalities are known concerning the RELAP5 critical flow model:

- For subcooled conditions, the RELAP5-calculated flow is too large. Often, it is found that a discharge coefficient of about 0.8 is needed to predict break flow in representative geometries containing break nozzles with length-to-diameter ratios less than 1.0.
- For low-quality saturated conditions, RELAP5-calculated mass flow rates are too low, often by as much as 20%, even when a discharge coefficient of 1.0 is used.
- Higher-quality saturated conditions at the break plane, such as are approximated by the homogeneous equilibrium model, are well-simulated with RELAP5.



### 3.4.2 Boron Model

The boron model is implemented by specifying an initial boron concentration in one or more volumes of a hydrodynamic system. Boron is specified using the "b" digit of the volume initial condition packed control word "ebt." A value of b=0 indicates no boron is present, b=1 indicates boron is present and requires a boron concentration to be entered as a part of volume initialization specification.

The boron model provides for tracking boron concentrations from injection sites, around coolant loops, out of coolant breaks, and through reactor cores. The purpose of boron tracking usually is to find the boron concentration within the core to determine a corresponding reactivity feedback effect. Therefore, it is appropriate to invoke the boron model only in problems where core power is calculated using the reactor kinetics model and the core boron concentration is expected to vary. The RELAP5 boron model assumes that boron is present only in the liquid phase and is transported along with the liquid phase. The model should be considered only a first-order approximation of boron effects because simulations of some potentially important effects, such as boron plateout and precipitation, are beyond the capability of the model. Note also that implementing the boron model does not affect the assumed fluid properties (e.g., the fluid density).

The boron concentration may be used as a component reactivity for the reactor kinetics core power calculation either using the TABLE4 reactor kinetics option or through a separate reactivity entry using a table or control variable. Using the TABLE4 method involves the generation of a four-dimensional table describing the coupled reactivity effects of fluid density, fluid temperature, fuel temperature, and boron. The separate method considers the boron effect simply as an independent reactivity component. The user is cautioned that the boron model has not been applied extensively.

### 3.4.3 Non-condensable Model

The non-condensable model is implemented by specifying a non-condensable gas type on control card 110 and indicating a non-condensable quality on one or more volume initial condition cards. A mixture of non-condensable gases may be specified by indicating more than one gas type on card 110 and specifying their mass fractions on card 115. However, only one non-condensable gas type (or mixture) may be used in a problem, and if an accumulator component is used in the problem, the non-condensable gas must be nitrogen (or include nitrogen in the case of a mixture). Available gas types are argon, helium, hydrogen, nitrogen, xenon, krypton, and air.

The non-condensable model assumes the gas is tracked with the vapor phase. Furthermore, the resulting gas-steam mixture is assumed to be isothermal (i.e., the gas and steam are in thermal equilibrium). A total pressure is calculated for the gas-steam mixture; the partial pressure of steam is available as a standard output variable.

The user is cautioned that the non-condensable model has been used only in a limited number of applications. Experience has shown that initialization difficulties may be encountered when the  $t = 6$  option (in the volume initial condition packed word "ebt") is used to specify initial volume conditions with non-condensables. For this purpose, the  $t = 4$  option is recommended.

Further experience has shown that calculational difficulties may be encountered during periods when a mixture of non-condensable gas and steam is appearing or disappearing (i.e., at very small void fractions). Circumventing these difficulties has required the analyst to manually (e.g., on restart) insert or remove vapor to artificially aid its appearance or disappearance.

#### 3.4.4 Reflood Model

The reflood model is implemented by specifying a nonzero reflood condition flag on the fuel rod general heat structure cards (format 1CCCG000). As described in the user input data requirements manual (Carlson et al., 1990a), reflood may be initiated when the adjacent volumes are nearly voided, when dryout of the heat structure is calculated, or by user-specified trip. The reflood option must be specified when the heat structure geometry data are first described. Once described, the heat structure geometry for the reflood structures cannot be deleted or changed.

Reflood is a phase associated with a large break LOCA sequence. Because RELAP5 was developed primarily as a small break LOCA analysis tool, the reflood model has received only limited experimental assessment evaluation and independent application experience. Therefore, few recommendations regarding reflood simulation and option selection may be made at this time. The limited experience to date indicates the code time step control features may not be adequate to handle reflood problems. Also, the reflood model should not be invoked when wall condensation is important or when non-condensables are present.

#### 3.4.5 Crossflow Junction Model

A hydrodynamic cell is interconnected with other cells through junctions at the cell faces. Because RELAP5 is a one-dimensional code, each hydrodynamic cell has two faces, at the inlet and outlet. The crossflow junction model was developed to circumvent some of the difficulties arising in applying a one-dimensional code in situations where multi-dimensional phenomena are present. The crossflow junction model allows connecting junctions at the cell centers in addition to the normal junctions at the cell faces. When using this capability to join vertical and horizontal components, it is recommended that the height of the vertical component be made consistent with the diameter of the horizontal component (however, the height of the vertical component should not be made less than 1 ft).

The crossflow junction is implemented using the "s" digit of the "fvcahs" junction packed control word. An  $s = 0$  indicator specifies a normal junction.  $s = 1$  indicates a crossflow junction where the "to" volume is a crossflow volume.  $s = 2$  indicates a crossflow junction where the "from" volume is a crossflow volume.  $s = 3$  indicates a crossflow junction where both the "to" and "from" volumes are crossflow. The crossflow option may not be specified for junctions associated with PIPE, JETMIXER, VALVE, and PUMP components. For ACCUM components, the  $s = 2$  and  $s = 3$  options are not allowed.

While the crossflow option provides a tool to simulate flow behavior in multidimensional flow geometries, a crossflow-linked model does not provide a full three-dimensional modeling capability because the momentum flux term is ignored for crossflow junctions. Therefore, it is recommended that the crossflow junction be avoided in locations where the transverse (crossflow

junction) velocity is comparable to or greater than the longitudinal (normal junction) velocities. Suggested applications of the crossflow model are presented in the following examples:

#### Example 1--Right Angle Connections

The connection of a PWR pressurizer surge line to the hot leg is a logical application for the crossflow model. The surge line in many plants enters the top of the hot leg at a right angle. During normal operation, the surge line flow is nearly zero while the hot leg flow is large. In most accident simulations, the pressurizer outsurge rate is small compared to the hot leg flow. Furthermore, since the entry is at a right angle, the momentum of any entering surge line flow does not have a component in the axial hot leg direction.

A suggested nodalization of the surge line/hot leg connection is shown in Figure 3-8. The local region of the hot leg is represented by components 100, 110, and 120; the pressurizer surge line is represented by component 550. As discussed previously, it is desirable to model the coolant loops symmetrically.<sup>a</sup> In the loops without the pressurizer, the piping corresponding to components 100, 110, and 120 may be lumped into a single pipe component. Symmetry may be maintained by sizing the loop components comparably. However, to accomplish this requires placing the center of a hot leg cell in each loop at the location corresponding to the pressurizer surge connection point. The user should therefore lay out the nodalization for the loop with the pressurizer first because it will define the nodalizations for the other loops as well.

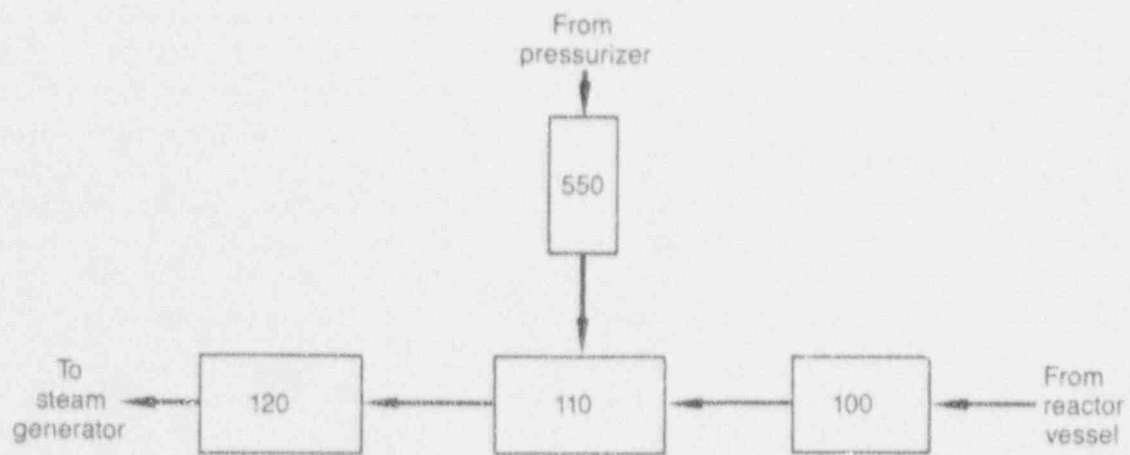
In Figure 3-8, components 100 and 120 might be single-volume components and component 550 might be a pipe. The connection would then be accomplished by using a branch for component 110. The branch would include three junctions with positive directions as indicated in the figure. Junctions 1 and 2 would be normal junctions at the inlet and outlet faces of cell 110. Junction 3 would be a crossflow junction, and a junction flag (fvcahs) of 0.0001 would be used. This junction is therefore specified as crossflow with component 110 representing the crossflow volume. The junction is specified as being on the top of the hot leg pipe. A full nonhomogeneous solution will be generated, the countercurrent flow limiting model is not operative, and the choking model is operative. Note the  $a = 0$  option has been selected. For crossflow junctions, the abrupt area change model is disabled (if selected, an  $a = 1$  flag is automatically reset to 0 by the code). Therefore the forward and reverse flow loss coefficients associated with a 90° tee should be determined independently by the user and manually input.

#### Example--2 Parallel Paths

Some simulation problems may involve relatively minor differences in otherwise similar parallel flow paths. These differences may result from geometrical or boundary condition differences. Consider, for example, a core with an inlet flow blockage affecting 25% of the core cross section. To model this situation, the core region may be subdivided into "blocked" and

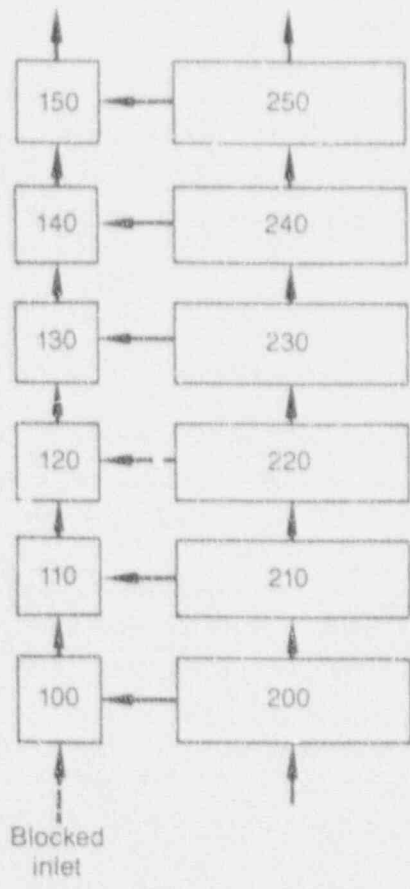
---

a. Although many plants and experimental facilities are symmetrical, some facilities are not symmetrical. Loop nodalization for nonsymmetrical facilities should be completed on a loop-specific basis.



1-6976

Figure 3-8. Surge line/hot leg crossflow connection application.



1-6975

Figure 3-9. Crossflow-connected core application.



"unblocked" regions. An example nodalization to model this situation is shown in Figure 3-9. Components 100 through 150 represent the blocked region, 200 through 250 the unblocked region. Inlet flow enters only at component 200. The crossflow model may be used to cross-connect these parallel flow paths that are hydraulically similar. Normal junctions are used to connect the cells in the primary flow direction (e.g., 110 to 120); crossflow junctions are used to connect cells transversely (e.g., 110 to 210). Note that it is not possible to use pipe components in this application since crossflow junctions may not be connected to the internal pipe cells. With the nodalization shown in Figure 3-9, fluid mixing will occur between the "blocked" and "unblocked" regions of the core, providing a simulation of the flow distribution.

### 3.4.6 Countercurrent Flow Limiting Model

The CCFL model is a new model in RELAP5/MOD2 that was not available in previous code versions. The model has not been applied except for checkout and developmental assessment applications. The CCFL model should prove valuable for simulating countercurrent flow problems; with previous code versions, these phenomena were controlled by the standard RELAP5 interphase drag model.

Example applications where CCFL may be a controlling phenomena are

- U-tube steam generator reflux cooling mode. Condensate inside the U-tubes must flow out of the tubes against steam flowing to be condensed. CCFL likely at the tube inlets.
- U-tube steam generator liquid holdup. When natural circulation loop flow is lost during a LOCA, draining of the U-tube upflow leg is opposed by steam flow. CCFL is likely at the tube inlet and in the vertical section of the hot legs.
- Once-through steam generator auxiliary feedwater penetration. Feedwater injected at the top of the tube bundle must penetrate downward into the bundle against steam flow from the lower bundle region. CCFL likely at the broached-hole tube support plates.

The CCFL model is implemented at a junction by specifying  $f = 1$  in the "fvcahs" packed junction control word. The Wallis and Kutateladze CCFL correlations (and a Bankoff weighting of the two) are available. The desired correlation and parameters are specified on the optional junction CCFL data cards. These cards are of the format CCC1401-CCC1499 for pipe component junctions, CCC0110 for single-junction and valve components, CCCN110 for branch component junctions, CCC0110 for pump inlet junctions, and CCC0111 for pump outlet junctions. In these formats, CCC is the component number and N is the branch junction number.

While the junction CCFL data card is termed "optional," the junction hydraulic diameter is specified on the card. If the card is not input, then a default junction hydraulic diameter, based on a circular junction flow area, is used. For noncircular geometries, and for "lumped-loop" situations, the code-calculated default junction hydraulic diameter will not be correct. The junction hydraulic diameter is used in the formulation of interphase drag for all junctions, not just at junctions where the CCFL model has been implemented. Because of this, the word "optional"

should be interpreted "required for all junctions where (a) the default hydraulic diameter is not acceptable or (b) the CCFL model is implemented."

### 3.4.7 Control System Modeling

RELAP5 control variables provide a general capability for modeling interactions among the various types of calculated parameters. Control variables may be used to relate the condition of thermal-hydraulic variables (e.g., temperatures, pressures, and flow rates) with the status of trips. Control variables also provide a general data manipulation capability. Calculated data may be summed, multiplied, divided, differentiated, integrated, lagged, or raised to a power. Because the responses of the control variables may themselves be interrelated, the response of an actual control system may be simulated.

In a RELAP5 problem, control variables are typically employed in three types of applications: (a) to include useful "side" calculations in a problem, (b) to specify complex boundary conditions, (c) to simulate the response of a prototype control system during a calculation. Examples of these types of applications are provided in the following sections. Specific descriptions of the control variable types and details of the input required appear in Section 4.11.

**3.4.7.1 Useful Side Calculations.** Control variables let the user manipulate data during a calculation and display the resulting response in the printed and plotted output. These data manipulations during the calculation often aid analyst understanding and reduce post-processing effort.

Examples where side calculations may be useful include tracking of steam generator secondary side mass, integrated injection flow, integrated break flow, and total steam generator heat transfer rate. In some instances, these data manipulations can be performed following the calculation by operating on the data file. For integrated data, the side calculation is necessary or the correct data will be lost.

To illustrate situations where side calculations are needed, consider the integrated break flow parameter. A side calculation of integrated break flow is included in the problem (through an integral control variable operating on the break junction mass flow rate). The integrated break flow will be calculated during each time step of the problem and its value will appear on the calculation restart/plot file. The frequency of the data points on the restart/plot do file will be the minor edit frequency. If this side calculation is not included in the problem, then integrated break flow must be approximated by integrating the minor edit mass flow rate data using a post-processing routine. However, the true integrated break flow data are lost because the data on the restart/plot do not include the time steps between the minor edits. Therefore, if a side calculation is not performed during the calculation, the integrated data are lost. To recover it would require rerunning the problem with the side calculation implemented.

An example of using control variables for side calculations is shown in Figure 3-10. In this example, control variable 7 has been developed to calculate the mass on the secondary side of a steam generator. The control variable adds the products of the densities and volumes of each of the 14 hydrodynamic volumes in the model of the steam generator secondary. The densities are

```

S*****
S steam generator c secondary side mass
S*****
*
*clivar      name      type      factor    init    f c
20500700    "sgcmass"    sum      2.2046    93260    0 0
*
*clivar      a0      coeff      variable name  parameter no.
20500701      0.0      15.52      rho            454010000
20500702      0.0      5.11       rho            458010000
20500703      0.0      3.88       rho            462010000
20500704      0.0      1.26       rho            462020000
20500705      0.0      1.26       rho            462030000
20500706      0.0      0.97       rho            462040000
20500707      0.0      7.65       rho            466010000
20500708      0.0      10.26      rho            466020000
20500709      0.0      10.40      rho            466030000
20500710      0.0      10.74      rho            466040000
20500711      0.0      10.73      rho            470010000
20500712      0.0      14.17      rho            474010000
20500713      0.0      19.75      rho            478010000
20500714      0.0      19.88      rho            482010000
S*****

```

Figure 3-10. Example of using control variables for side calculations.

accessed through the specification "rho" followed by the identifier of the hydrodynamic volumes. Note that references to these densities will be SI in units (in this case,  $\text{kg/m}^3$ ) regardless of the units specified for the problem on the units selection control card 102. Overlooking this fact is a common cause of modeling error. Accordingly, in this example, the volumes of the hydrodynamic cells are specified in  $\text{m}^3$ . Since this model was based on British units, the resulting mass in kg is converted to lbm using the conversion factor 2.2046 on card 20500700. Note the descriptive name "sgcmass" is specified to recognize the control variable information in the printed output.

**3.4.7.2 Specifying Complex Boundary Conditions.** Control variables may be used to impose virtually any boundary condition on a problem. Boundary conditions may be tailored to suit the calculation desired based on user input (e.g., from a table), the current status of any variable in the problem, or a combination of these factors.

To illustrate the power of control variables for specifying boundary conditions, consider the following example. Fluid inventory in a plant system is controlled by makeup and letdown systems; makeup injects fluid and letdown extracts fluid. In the plant, the letdown flow is returned to a 2000-gal makeup tank through a cleanup system. During normal operation, the makeup and letdown flows are balanced. In the model, however, these systems are modeled as "open loop." The makeup system was modeled using a pump that draws fluid from a TMDPVOL, and the letdown system was modeled using a trip valve that allows flow into another TMDPVOL. The decision to use an open loop model rather than a comprehensive closed loop model of the system was made because of the complexity of the cleanup system and incomplete information on its details. Moreover, in this particular case, complete modeling of the cleanup system was deemed unnecessary and representing it with the boundary conditions was considered adequate.

With the open loop modeling concept, however, a dilemma arises. During a transient, the letdown flow will be terminated and the makeup system will draw down the inventory in the makeup tank. When the tank is empty, the makeup flow will cease. By employing the control variables and trips shown in Figure 3-11, this makeup flow termination was realistically included in the simulation.

Trip 550 is used to determine the letdown status. Letdown flow is to be terminated when the pressure at the core inlet (p 505010000) falls below 3.42178 MPa. Prior to that occurrence, trip 550 is false, afterwards it is true. The status of this trip is used to control the letdown valve position. The valve is open when trip 550 is false and closed when trip 550 is true. Valve control is accomplished by using a trip valve that references the inverse of trip 550 (specified as -550).

Trip 550 also is used to provide a binary indication of letdown isolation; this is accomplished with trip unit control variable 801. As shown in Figure 3-11, this control variable will have a value of 0 until trip 550 latches true (when letdown is isolated) and a value of 1 thereafter.

Control variable 802 is defined as the mass flow rate of the makeup injection junction (mflowj 850010000). Control variable 803 is defined as the product of the mass flow rate and the binary operator (control variable 801  $\times$  control variable 802). Control variable 803 thus has a value of 0 up to the time of letdown isolation, then a value equal to the makeup injection mass

```

*-----*
*          trip input          *
*-----*
0000550  p  505010000 lt null 0 3.42178e6 1 -1. *letdown isolation
0000551  cntrlvar 804  gt null 0 2258.4 1 -1. *mu tank empty
*-----*
*          control variable input          *
*-----*
*cntrlvar  name      type      factor  init  f c      min  max
20580100  "binary"   tripunit  1.    0.    0 3      0.   1.
*
*cntrlvar      trip no.
20580101      550
$-----$
*cntrlvar  name      type      factor  init  f c      min  max
20580200  "flow"      sum      1.    14.4792 0 0
*
*cntrlvar      a0      coeff      variable name  parameter no.
20580201      0      1.      mflowj      850010200
$-----$
*cntrlvar  name      type      factor  init  f c      min  max
20580300  "flow"      mult     1.    0.    0 0
*
*cntrlvar  variable name  parameter no.  variable name  parameter no.
20580301  cntrlvar      801          cntrlvar      802
$-----$
*cntrlvar  name      type      factor  init  f c      min  max
20580400  "inflow"   integral  1.    0.    0 0
*
*cntrlvar      integrand name  integrand no.
20580401      cntrlvar      803
$-----$

```

Figure 3-11. Example of using control variables for specifying complex boundary conditions.



flow rate (in kg/s) thereafter. Control variable 804 integrates control variable 803; as a result, the value of control variable 804 represents the integrated makeup injection flow subsequent to letdown isolation. Using trip 551, the value of control variable 804 is compared against 8358.4 kg (the mass equivalent of the 2000-gal initial tank inventory assuming constant temperature and pressure in the tank). When the integrated injection flow exceeds this value, trip 551 turns true and is used to trip the power to the makeup injection pump.

**3.4.7.3 Modeling Prototype Control Systems.** Control variables may be used to model virtually any prototype control system. Control systems modeling generally is limited by the availability of control process diagrams and information on the actual set points and gains, rather than by the capabilities of the RELAP5 control variable models.

To illustrate the use of control variables for modeling prototype control systems, consider the following example. This example models a prototype pressurizer level control system. The control system determines a pressurizer indicated level based on the difference between the pressures sensed at pressure taps near the bottom and top of the pressurizer. The indicated level is first lagged, based on instrument response time, and then compared against a "set point" level that varies as a function of the highest average (of the hot and cold leg) temperature of the three coolant loops in the plant. The resulting error between the indicated and set point levels is processed through a proportional-integral controller whose output is used to vary the makeup pump speed. If the level indication is low, the control system response is to increase the makeup flow to correct it.

The control variable logic shown in Figure 3-12 was developed to model the response of the system described in the preceding paragraph. Control variable 200 determines the set point level as a function of the highest average temperature. In previous logic (not shown), the hot and cold leg fluid temperatures in each of the three loops were independently averaged and an auction process selected the highest of the three average temperatures. In the example, this highest average temperature was previously defined using control variable 104. The coefficients prescribed in control variable 200 operate on this temperature to define the pressurizer set point level. Initially (assuming full power temperatures), the set point level is 0.533, or 53.3% of full scale.

Control variable 201 calculates the pressurizer indicated level based on the difference between the pressures at the elevations of the prototype pressure taps. In this example, the location of the lower tap was defined to be at the center of hydrodynamic cell 341070000. However, the elevation of the upper tap was between the centers of two of the cells in the model (341010000 and 340010000). Thus, the pressure at the upper tap is based on an elevation-weighted average of the pressures in these two cells.

The instantaneous value of the pressurizer indicated level (control variable 201) is lagged, based on the response time of the instruments, in control variable 202. The level error is then determined by subtracting the lagged indicated level from the set point level in control variable 203. In turn, the level error is processed by the proportional-integral operator in control variable 204. The output from this processor is a change in makeup pump speed. If the makeup pump is

```

*****
the following control variables - 200 through 206 - represent the
Sprussurizer level control system
*****
*
*ctlvar      name      type      factor      init      f c      min      max
20520000 "prz sp lvl"  sum      1.0        0.533     0.3      0.222  0.533
*
*ctlvar      a0      coeff      variable name  parameter no
20520001      -6.03230  1.14338e-2  cntrlvar      104
*****
*ctlvar      name      type      factor      init      f c      min      max
20520100 "prz dp lvl"  sum      1.0        0.227118  1.3     0.0     1.0
*
*ctlvar      a0      coeff      variable name  parameter no
20520101      -0.20759  2.21849e-5  p              341070000
20520102      -1.18443e-5  p              340010000
20520103      -1.03406e-5  p              341010000
*****
*ctlvar      name      type      factor      init      f c      min      max
20520200 "prz level"  lag      1.0        0.227118  1.3     0.0     1.0
*
*ctlvar      tau-1      variable name  parameter no
20520201      0.786      cntrlvar      201
*****
*ctlvar      name      type      factor      init      f c
20520300 "prz lsp-1"  sum      1.0        0.0       0
*
*ctlvar      a0      coeff      variable name  parameter no
20520301      0.0       1.0       cntrlvar      200
20520302      -1.0      -1.0      cntrlvar      202
*****
*ctlvar      name      type      factor      init      f c      min      max
20520400 "cvcs d rpm" prop-int  10.0     0.0       0.3     -0.50649  3.0
*
*ctlvar      prop gain  int gain  variable name  parameter no
20520401      1.0       5.55556e-3  cntrlvar      203
*****

```

Figure 3-12. Example of using control variables in modeling actual control systems.

modeled explicitly, control variable 204 is then used to modify the pump speed on each time step. If, instead, the makeup system is simply modeled using a TMDPJUN, the effect of the change in pump speed is correlated into a corresponding change in flow and the junction flow is modified accordingly.

## 4. SPECIFIC PRACTICES

This section discusses practices for applying RELAP5. Specific guidance is provided for applying each of the submodels in the code. The discussion is organized in the same order as the list of input requirements in the user input section of the code manual (Carlson et al., 1990a). The organization generally also follows the recommended sequence of data in an input deck.

### 4.1 Problem Control Options

The following sections describe the various problem control options that are selected by a series of control cards. For convenience, it is recommended that these cards appear at the beginning of an input listing.

#### 4.1.1 Format Considerations

Input data typically are submitted using an 80-column format. It is recommended that the first card of an input stream be the title card. A title card is identified using an equal sign as the first non-blank character. It is recommended that the title card be descriptive of the input stream. A descriptive title might specify the facility, the purpose of the deck, and an additional identifying feature such as a date. To illustrate, consider the title: "=Zion-1 PWR, full power steady state, 1-30-90." In addition to its appearance at the beginning of the input listing, the title specified will also appear as a heading on the major edits in the printed output.

Despite the effort involved, it is highly recommended that input streams be well-commented. Comment cards may be inserted at any location in an input stream by using an asterisk or dollar sign as the first non-blank character on a data card. Comments may also be appended following the entry of data on any card by using either of these characters. All fields on the card following an \* or \$ are read as comments by the code.

The card identification number, the first entry on each card, is the key to code interpretation of the data entered on the cards. It is recommended, but not necessary, that the input data stream be organized by increasing card number. Input of real numbers may be accomplished using any standard FORTRAN notation (e.g., acceptable inputs for the number 12.45 include +12.45, 0.1245+2, 1.245+, 1.245 1, 1.245E+1, and 1.245D+1). Alphanumeric entries with embedded blanks must be enclosed using quote (") or apostrophe (') delimiters. Data may be continued from one card to another using a plus sign (+) as the first field of the next card (a card number is not required on the continuation card). Data fields must be complete on each card (i.e., a field cannot be started on the original card and completed on the continuation card). Where possible, it is recommended that continuation cards not be used to increase analyst understanding of an input stream and reduce interpretation errors.

The input stream is terminated with a card containing a period or forward slash as the first entry. The data input stream is therefore limited to all data preceding the terminator card (note that the title card, identified by the equal sign, does not need to be the first card of the input

stream). To highlight the presence of the terminator card, it is recommended that it be commented (e.g., " \*end of input").

The sequential expansion format for data entry is described in Section A-1.8 of the input data requirements manual (Carlson et al., 1990a). This format provides an efficient method for entering certain data and it is recommended that it be used where available.

#### **4.1.2 Problem Type—Card 100**

The most common RELAP5 calculation types are NEW, RESTART, and STRIP. The NEW option is used for problems where a complete input stream is specified. With this option, initial conditions for all model features (e.g., volumes, junctions, heat structures, control variables, and trips) must be specified on the input cards.

The RESTART option is used where a previous calculation (either NEW or RESTART) has been performed and the current problem is to be an extension of that calculation. A RESTART calculation may be simply an extension of a previous calculation. If this is the case, the input stream only needs to contain the control cards to effect the continuation of the problem. Often, however, changes in the model are desired at the time of restart and RELAP5 offers considerable flexibility for making such changes. Virtually any model change may be made when restarting a previous problem. To effect a change, the model feature is simply re-input as a part of the restart problem input stream. Any changes made are considered permanent (i.e., once a change is made it will remain a part of a problem unless further modified in a later restart run). Conversely, any model feature not changed in a restart calculation is assumed to exist as originally or last specified and is initialized based on the conditions present at the restart time from the preceding calculation. When making changes on restart, care should be taken to ensure that the initial conditions of the features changed are consistent with those from the original problem at the restart time. Care should also be taken to determine all possible effects of any changes made.

The STRIP option is used as a post-processor for "stripping" the data for a limited number of data channels (e.g., 10 pressures, 15 temperatures, 14 flow rates, and 10 control variable values) from the restart/plot file. The strip option is used to create a file containing only pertinent data. This new file is therefore of a more manageable size than the restart/plot file. Considerable efficiency is gained by stripping the desired data; the memory requirement for an external plotting routine and the computer time required to execute it are both reduced.

For NEW problems, either the TRANSNT or STDY-ST options may be used. For reasons discussed in Section 3.1.3.2, it is recommended that the STDY-ST option not be used.

#### **4.1.3 Input Check/Run—Card 101**

This optional card allows the user to stop a calculation following completion of input processing and before execution of a transient or steady-state problem solution. If card 101 is not present, the RUN option is assumed; if the card is present, RUN or INP-CHK may be selected.



As described in Section 3.1.2, stopping a calculation after successful completion of input processing may have some benefit as a part of the model debugging process. It is recommended, however, that models be debugged in the TRANSNT mode using the RUN option, being careful to specify an appropriate maximum computer usage time on card 105 (see Section 4.1.6). With this method, the model input is iteratively debugged in the RUN mode (input processing routines are the same in the RUN mode as in the INP-CHK mode). When all input errors have been removed, an initial transient calculation is automatically performed. This initial transient calculation often provides an advance indication of additional modeling errors beyond those that can be diagnosed by the RELAP5 input processor. If the input check option is used, a separate computer job is required to start the transient or steady-state calculation.

#### 4.1.4 Units Selection—Card 102

Optional card 102 lets the user specify the calculational units for a problem. SI units are assumed if card 102 is not input. A units specification is made for both the input (model input stream) and output (printed).

Several peculiarities of the units assumed by the code are described in Section A-2.3 of the user input data requirements manual (Carlson et al., 1990a). Additionally, the user should carefully consider the input units requirements specified in the same manual. These requirements are identified in parentheses next to each input listing.

All internal RELAP5 calculations and all data storage on the restart/plot output file are in SI units, regardless of the options selected on card 102. The user is cautioned of two situations where unit difficulties may arise. Note that both these difficulties may be avoided if a problem is performed using SI units exclusively; therefore, if at all appropriate, SI units are recommended.

First, references to code parameters within control variable specifications are considered an internal code calculation and SI units are assumed. For example, in a control variable reference to p 120010000, the pressure in cell 12001 will always be returned as pressure in Pascals. The control variable specification provides sufficient capability to convert to British units if the user desires. Difficulties arise, however, if a problem is being performed in British units and the user fails to remember that the code internal units are SI.

Second, all data written to the restart/plot file are in SI units. Conversion of an output channel to British units therefore requires a STRIP calculation followed by an external conversion of British to SI units.

#### 4.1.5 Restart Control—Cards 103 and 104

For a restart problem, the restart number from a previous calculation is specified on card 103. The number to place on this card is the "restart number" (not the "block" number) appearing in a restart edit of the previous calculation's printed output. When a restart edit is generated at the same time as a major edit the restart data appear after the major edit data. Card 104 provides a mechanism for preventing the writing of a restart/plot file if so desired.

A restart problem is simply an extension of a previous calculation, beginning from the exact conditions present at a restart edit in that calculation. Note that the previous calculation may be restarted from its end point (a restart edit is automatically generated when a calculation terminates) or any previous restart edit. The user is cautioned, however, that the restart edit created when a calculational failure occurs is unreliable as a restart point because the calculated parameters reflect the failed conditions. For restarting following a code failure, the user must use the restart edit previous to the terminating edit. Therefore, good practice includes specifying frequent restart edits so that code failures may be circumvented without extensive recalculation. However, this practice can result in very large restart files. If the calculation seems to be running smoothly, the restart edit frequency can be decreased.

A restart problem may be run "as is" (i.e., all features of the problem remain the same) or changes may be made in the model or its conditions at the time of restart. Any changes made upon restarting become a permanent part of the problem and do not need to be respecified on subsequent restarts. A restart input deck is quite abbreviated, consisting only of problem control cards, time step control cards, and cards specifying any changes desired. Virtually any change may be accomplished at the time of restart. Generally, to effect a change in a model feature it is necessary to reinput all cards needed to specify that feature. For example, if the volume of a single-volume component needs to be changed, then all cards needed to input that single volume must be reinput even though only one variable is changing. When reinputting data at a restart point, the user is cautioned to carefully respecify its initial conditions. These are shown in the major edit data at the restart point (for this reason, it is recommended that the same frequencies be specified for restart and major edits).

#### 4.1.6 Central Processing Unit Time Control—Card 105

Optional card 105 provides a means for terminating a calculation internally to RELAP5, based on the approach to a computer time usage limit. The use of this card is highly recommended to promote a "normal" termination. If a calculation is terminated externally (because, for example, the computer time expended reaches the maximum specified on an external job card) then a loss of the output data is likely. Card 105 provides a means of terminating a job based on an internal central processing unit (CPU) time limit. If required by the operating system, an external time limit is set to be higher than the internal time limit.

Three inputs are needed on card 105. Words 1 and 2 are time differentials (word 2 should be larger than word 1) and word 3 is the maximum CPU time allowed. Following each time step, a check is made to determine if the CPU time used to that point is greater than word 3 minus word 1. If so, the calculation is terminated immediately. A test is also performed to determine if the CPU usage has reached a value of word 3 minus word 2. If so, the job is terminated when the calculation has progressed to the next time corresponding to a minor edit point.

As an example, consider a calculation that a user would like to span a transient time from 0 to 100 seconds. Based on experience, the user believes the calculation will require about 500 CPU seconds. To run this calculation, the user will use an end time of 100 seconds on the last of the 2XX time step control cards. On card 105, the user might input the times 10, 20, and 700. On the external job card, an 800-second time limit might be specified. By doing this, the user has maximized the opportunity for a successful run to 100 seconds while limiting the exposure to

excessive computer costs if the calculation proves to proceed less efficiently than expected. First, the user has likely provided sufficient time for the calculation to reach the 100-second transient time. By specifying a maximum internal limit of 690 CPU seconds (700 - 10), the run will be terminated internally and therefore output files will be orderly. The user has provided 10 CPU seconds (20 - 10) to reach the next minor edit point once 680 CPU seconds have been expended. Therefore, it is likely that either the problem will be executed to completion, or if not, a fully-useful restart point will be generated to facilitate continuation of the problem.

An estimate of the CPU time needed to perform a calculation may be made by starting with a known reference point (i.e., the time needed to run a similar problem on the same computer) and linearly scaling the CPU time (a) proportionally by the number of hydrodynamic cells in the problem, (b) proportionally by the requested problem time, and (c) inversely proportional by the requested or expected time step size. As indicated above, if the user has a reasonable estimate of the CPU time required for his problem, then considerable efficiencies in the execution of the problem are possible.

#### **4.1.7 Non-condensable Gas Type—Cards 110 and 115**

These cards specify the presence and composition of a non-condensable gas. The user input requirements document description for these cards is self-explanatory (Carlson et al., 1990a). The user is cautioned that the non-condensable model has only limited user experience. A basic description of the non-condensable model appears in Section 3.4.3.

#### **4.1.8 Hydrodynamic System Definitions—Cards 12X**

These optional cards enable the user to specify the working fluid within each independent hydrodynamic system in a model. For systems employing only light water (as is most commonly the case), these cards are not required. For situations where other fluids are used, one card should be entered for each independent hydrodynamic system in the model. The word "independent" implies that there is no possibility of flow between the two systems. For example, the primary and secondary systems of a steam generator are normally independent systems. However, for the simulation of a steam generator tube rupture event when the two systems are hydraulically coupled through a break path, the two systems are no longer independent. Flow between systems using different working fluids is not allowed with RELAP5.

Currently available working fluids are light water (specified as WATER), heavy water (D2O), and hydrogen (HYDROGEN). The user is referred to the cautionary notes regarding this input in Section A-2.11 of the user input data requirements manual (Carlson et al., 1990a).

#### **4.1.9 Self-Initialization Options—Cards 140 through 147**

A common modeling task, and one that can consume excessive time and funds, is obtaining a satisfactory steady-state condition for a system model. A steady initial condition usually is needed as a starting point for transient calculations. Standard controllers have been installed into RELAP5 to facilitate the calculation of a PWR steady operating condition. These standard controllers are referred to as the "self-initialization" options.

The self-initialization options are invoked by entering cards 140 through 147. These options provide for specifying pump, steam flow, feedwater flow, and pressure controllers. The numbers of each type of controller are described on card 140. The remaining cards indicate the components where the control is to take place and a reference to a control variable where the requisite constants and functions are calculated and stored. Cards 141 and 142 provide this information for the pump controllers, cards 143 and 144 for the steam flow controllers, cards 145 and 146 for the feedwater flow controllers, and card 147 for the pressure controller. Detailed information explaining the use of control variables is found in Section 4.10.

The application of the self-initialization controllers for a typical (U-tube type steam generator) PWR steady operating condition is briefly described as follows. To begin, a constant core power is input using a table entry. The primary coolant system pressure is controlled using a pressure controller at a location where the pressure is well known (e.g., in the pressurizer or at the core outlet). Pump controllers are used to adjust the primary coolant pump speeds so that the desired core flow rate is maintained. In most cases, the coolant loops are identical; therefore all primary coolant pumps are driven at the same speed. The feedwater injection flow rates are controlled so that set point steam generator indicated levels are maintained.

The steam flow controllers may be used in two different ways, both of which result in the total heat transfer rate through the U-tubes of all steam generators equaling the core power. First, the steam flow may be adjusted based on the cold leg temperature error. With this method, the resulting steady state will possess the proper hot and cold leg temperatures but the steam generator secondary pressure may not be as desired. Second, the steam flow may be adjusted such that the desired steam generator secondary pressure is attained. With this method, the resulting steady state will possess the proper steam generator secondary pressures, but the hot and cold leg fluid temperatures may not be as desired. The modeling difficulty reflected here primarily concerns the calculation of the heat transfer process on the secondary side of the U-tubes. Specifically, flow patterns in the tube bundle region are highly complex.

The code-calculated heat transfer coefficient on the outside of the tubes is generally too small. As a result, when the primary-side temperatures are correct, the secondary-side pressure needed to remove the core power is too low. A model adjustment that has been found effective for correcting this disparity is to adjust the heated diameter specified on the secondary-side of the tubes. If the classically-calculated heated diameter (i.e., four times the flow area divided by the heated perimeter) is replaced with the tube-to-tube spacing, then good agreement with plant data is obtained for both the primary-side fluid temperatures and the secondary-side pressures. Here, the meaning of "tube-to-tube spacing" is the minimum fluid gap width between the outside surfaces of two adjacent steam generator tubes. Note that this recommended change affects only the heated diameter specified on the outer tube surface; no change is made to the hydrodynamic volume hydraulic diameters.

The selection of appropriate gains for the various controllers is largely a trial-and-error process. An initial gain is selected, the controller response is monitored, and the gain is adjusted based on any indications of under- or over-damping. In the terminology of the self-initialization controllers, the integral part of the time constant is the inverse of the gain. Therefore, an increased gain results in a smaller time constant and more rapid controller response.



A complete discussion of the self-initialization controllers may be found in *Self-Initialization Option for RELAP5/MOD2* (Johnsen et al., 1986). The user should note that these controllers have potential for uses other than the self-initialization of a model. For example, the pump controller may simplify the modeling of a pump whose speed is controlled based on a complex combination of inputs.

## 4.2 Time Step Control

Cards 200 through 299 are the time step control cards.

Optional card 200 lets the user define a problem time other than zero at the beginning of a NEW type problem. This is a very useful feature because a problem start time can be normalized to any convenient reference. Examples where this capability is needed include resetting the problem time to zero when a satisfactory model steady initial condition has been attained and normalizing the problem start time with a nonzero reference time in external data, such as when simulating an experiment that starts at 200 seconds.

Cards 201 through 299 contain data that control the time steps used and the output generated as a problem progresses. At least one card is needed for NEW problems. For RESTART problems, if these cards are input they replace the entire series of 201-299 cards in the preceding calculation. It is generally recommended that at least one 201-299 card be entered in RESTART problems.

Seven words are entered on these cards. Word 1 defines the end time of the interval for which the data in the following words is used. The calculation proceeds either from time zero, from the restated initial time on card 200, or from the restart time and proceeds to the time specified in word 1 of card 201. When that time has been reached, control of the problem is based on the data on card 202, and so on until the time on the last of cards 201-299 is reached when the job is terminated. Regardless of the specifications provided in words 2 through 7, minor edit, plot, major edit, and restart edits are generated by the code at the end of every time interval specified on a 201-299 card.

Word 2 on the 201-299 cards represents the minimum time step. From experience, a value of  $1.0E-7$  seconds is recommended. Using the default  $1.0E-6$  second default value occasionally causes calculational difficulties. While smaller values may be needed in some applications, for economic reasons the user will want to first verify that such a small value is warranted.

Word 3 represents the maximum (or requested) time step. If calculational difficulties are encountered, a reduction in the maximum time step size often remedies them. A maximum time step size of the Courant limit (but not larger than 0.2 seconds) is recommended. A discussion of time step selection appears in Section 3.1.3.1.

Word 4 is the packed-word "ssdtt" that specifies the code control and output functions. In general, the option 00003 (or simply 3) is recommended. A short discussion of how this option may be varied to obtain expanded data output for problem diagnoses appears in Section 3.1.3.1.



Words 5, 6, and 7 specify the minor, major, and restart edit frequencies as integer multiples of the maximum time step size from Word 3. For example, with a maximum time step size of 0.1 s, a minor edit frequency of 10, a major edit frequency of 100, and a restart frequency of 200 then the code will generate minor edits every 1 s, major edits every 10 s, and restart points every 20 s.

It is recommended the user select a minor edit frequency for an appropriate plot output frequency, a major edit frequency for an appropriate phenomena "snapshot" frequency, and a restart edit frequency for an appropriate "backup following failure" frequency as described in Section 3.1.3.1.

## 4.3 Minor Edit and Expanded Edit/Plot Variable Requests

### 4.3.1 Minor Edit Requests

Cards 301 through 399 are reserved for minor edit requests. Requesting a minor edit simply results in a display of the specified parameter in the printed output. As described in the previous section, the minor edit data will be printed at an interval prescribed on the 201-299 cards; the interval is defined by the product of the maximum (or requested) time step size and the minor edit frequency. The frequency of data entries on the restart/plot file will be the same as for the printed minor edits. However, it is a common misconception that a data channel must be requested as a minor edit variable in order to have that data written to the restart/plot file. Data for virtually all calculated parameters (exceptions are discussed in Section 4.3.2) are written to the restart/plot file regardless of what, if any, minor edit requests are specified.

The minor edit request is entered by a card number from 301 to 399 followed by two fields that specify the data channel. For most data these fields reflect the data type and data location. For example, the pressure in cell 3 of pipe component 125 would be specified as "p 125030000".

Two common input errors are encountered when specifying minor edits. First, when requesting the "Component Quantities" listed in Section A-4.2, the location identifier is simply the component number, not the typical cell number as was used in the example above. When requesting the pump velocity for pump component 255 the proper specification is PMPVEL 255. A common error is to request "PMPVEL 255010000," a format that is consistent with requesting most other data about the pump (such as pressures and void fractions). Second, input errors often result because the proper specification for junction data (such as mass flow rates, velocities, and void fractions) is not consistent for all types of components. If only one junction is associated with component number CCC (single-junction, valve, time-dependent junction, and accumulator components include only one junction) then the junction location is identified with the format CCC000000. If more than one junction may be associated with component CCC [pipe/annulus, branch/separator/jet-mixer/turbine/emergency core cooling (ECC) mixer, pump, and multiple-junction components may include more than one junction], then the proper format is CCCNN000. NN is the junction number within the component.

If minor edit requests have been entered in a NEW calculation, then they need not be re-entered on subsequent RESTART calculations. The originally-requested minor edits will appear in the output of the restart calculations. If, however, a change in the minor edit requests

is made when a calculation is restarted (e.g., by adding more requests), then the entire block of desired minor edit request cards must be re-input in the restart job input stream.

It is recommended that the user employ minor edits as a useful analysis aid. In a newly assembled input deck, it is desirable to assemble a list of minor edit requests to characterize overall behavior in the model. This list might include representative pressures, temperatures, flow rates, and velocities in the important regions of the model. The list should also include the current values of any especially important control variables. In a mature input deck being used for transient calculations, the minor edits should be tailored for interpreting the transient behavior calculated. For this purpose, the minor edit request list would highlight parameters such as core power, break flow, and fuel temperatures.

#### 4.3.2 Expanded Edit/Plot Variable Requests

A new feature in RELAP5/MOD3 is the capability to request that certain nonstandard additional data be printed as minor edits and added to the restart/plot file. A list of these additional data is given in Section A-4.8 of the user input data requirements document (Carlson et al., 1990a).

Additional data are requested by entering cards of the format 2080XXXX, where XXXX may range from 0001 to 9999. One card is used for each additional parameter and two words are entered comparably to those on the 301-399 cards. Note that these parameters are not written to the restart/plot file, nor are they usable references in control variables, minor edits, or trips, unless they are included on a 2080XXXX card.

On the additional data list, two items are of particular interest to the user. The "HTMODE" request code, followed by the appropriate parameter number, may be used to access the heat transfer mode calculated on a surface of a heat structure. This information is not available in the standard data list. The "HTTEMP" request code, followed by the appropriate parameter number, may be used to access the calculated temperature for any node in a heat structure. Without this request, only the left and right surface heat structure temperatures are stored on the restart/plot file.

### 4.4 Trips

Trips are binary logical operators whose status at each time step is either true or false. The value of a trip statement is that it allows this binary type of data to be fully incorporated into a calculation. A trip statement may access any calculated parameter (such as temperature, pressure, flow rate, and control variable value) and perform a comparison to judge whether the current status is true or false. Conversely, a trip status may be used to cause an action to occur in the problem (e.g., by opening a valve when a trip turns true).

RELAP5 employs two basic types of trips, variable and logical. The variable trip is used to compare one calculated parameter against another (or against a constant) to determine a true or false status. The logical trip directs a combination of other trips into a new trip whose status is either true or false. When assembling trip logic, the user should remember that trip status is determined at each time step in numerical order by trip number. As a result, if a lower number

trip is referenced in a trip statement, the status of the referenced trip is based on the current time step. Similarly, if a higher number trip is referenced, then the status of the referenced trip is based on the previous time step.

RELAP5 trip logic may be either in the original or extended format. The original format allows for 200 variable and 200 logical trips; the extended format allows for 1000 of each. The choice of format is dependent on whether the user anticipates a need for more than 200 of either type of trip. The original format is used unless the extended format is activated by entering the 20600000 card. Examples presented here are in the original format.

#### 4.4.1 Variable Trips

Variable trips, implemented using cards 401-599, are used to compare one calculated parameter against another or against a constant. To illustrate the variable trip concept and some of its possible uses, consider the following example:

```
505 p 140010000 gt p 145010000 50. n -1. *delta p
```

As a logical statement, trip 505 status is determined based on the question "is the pressure in cell 14001 greater than the pressure in cell 14501 by more than 50 psia?" If the answer to that question is yes, the current status of trip 505 is true, if not its status is false. The "n" (nolatch) specification means that the code asks this question during each time step to determine the status of the trip. With the alternate specification "l" (latch), the code continues to ask the question until the status of the trip is true. After that occurrence, the code stops asking and the status of the trip is assumed to be true thereafter. In other words, the trip has been "latched" true. The appended entry "-1." indicates the initial status of the trip (i.e., at the time card 505 is input to the problem) is false. If a positive number is input here, it is interpreted as "the time this trip last turned true." The data following the asterisk is simply a comment to remind the analyst of the purpose of trip 505, in this case a check of the differential pressure. Note that in this example, the 50 psia constant assumes the problem is run in British units; in problems run in SI units the constant would be interpreted as 50 Pa.

The status of trip 505 may be used to implement virtually any action into the model when the differential pressure exceeds 50 psia. For example, the occurrence of trip 505 turning true may be used to trip a reactor, trip a pump, initiate an injection flow, open a valve, or change the value of a control variable from 0 to 1.

A variable trip may also be used to compare the current value of any calculated parameter against a constant. To illustrate, consider the following example:

```
506 mflowj 560010000 lt null 0 500. l -1. *low flow
```

Trip 506 asks the question "Is the mass flow rate at Junction 56001 less than 500 lbm/s?" The initial status of trip 506 is indicated as false and if the statement is ever true, it will be latched true thereafter. This statement might be used, for example, to scram a reactor as a result of violating a flow rate limit, as suggested by the low flow comment.

In many modeling situations, it is desirable to input references to trips whose logic will be refined at a later time. For example, when entering data for a pump component, it is necessary to specify a pump trip number. When this trip is false, the pump is assumed to be driven by the pump motor; when it is true, a pump coast down is assumed based on the physical characteristics of the pump and motor and the interaction with the hydrodynamic phenomena.

The modeler may input a trip number of 0, but doing so increases the complexity of implementing a pump trip later. If the user wants to include a pump trip later, say as a function of pressure, it will be necessary to re-input the entire pump component in a restart job just to redefine the trip. If, instead, the modeler initially specifies a "dummy" pump trip, then the pump trip may be later incorporated into the model simply by replacing this trip's dummy logic with the actual trip logic in the restart job. The advantage to the modeler is that re-specifying the trip involves a single input card while re-specifying the entire pump component involves hundreds of cards.

A convenient method for specifying dummy trips is to simply provide a convenient "always true" or "always false" reference. To illustrate, consider the following trips:

```
507 time 0 lt null 0 1.e6 l 0. *always true
508 time 0 gt null 0 1.e6 n -1. *always false
```

Trip 507 is true at time 0 and will always remain true while trip 508 is false at time 0 and will always remain false (of course, this assumes that problem times beyond 1,000,000 seconds will not occur).

#### 4.4.2 Logical Trips

RELAP5 logical trips, implemented using cards 601-799, are used to combine the status of two trips using standard logical operators. These logical operators are AND, OR, and XOR. To demonstrate these operators, consider two variable trips, 520 and 521, and the logical trips 620, 621 and 622:

```
620 520 and 521 n -1.
621 520 or 521 n -1.
622 520 xor 521 n -1.
```

Trip 620 will be true only when the status of both trips 520 and 521 are true. Trip 621 will be true when trip 520 is true, when trip 521 is true, or when both trips 520 and 521 are true. Trip 622 will be true when either trip 520 or trip 521 is true, but not when both trips 520 and 521 are true. XOR is termed the "exclusive or" operator. The use of the latch/nolatch and initial value indicators in logical trips is the same in variable trips as described in the previous section.

In the examples shown above, the logical trips have only referenced variable trips. However, logical trips may also reference other logical trips. Furthermore, a logical trip may reference itself. When this is done, the logical trip is referencing its own status on the previous time step.



### Example 1 -- Reactor Trip Logic

As a demonstration of the capabilities of the RELAP5 trip logic, consider the reactor trip logic in the following example. Assume that a reactor trip occurs if any of the following conditions are met:

- The pressurizer pressure exceeds 2300 psia
- The pressurizer indicated level falls below 20%
- Any one of the three hot leg temperatures exceeds 610°F
- The operator initiates a manual reactor trip.

Also, assume that once a reactor signal has been generated there is a 0.5-second delay prior to movement of the scram rods. To include a simulation of this reactor trip behavior in a RELAP5 model, variable trips are first developed to provide the required parameter comparisons:

```
501 p      450010000  gt  null 0 2300.  1  -1.  *przr p
502 cntrlvar 100      lt  null 0 0.20  1  -1.  *przr level
503 tempf  110010000  gt  null 0 610.  1  -1.  *hl1 temp
504 tempf  210010000  gt  null 0 610.  1  -1.  *hl2 temp
505 tempf  310010000  gt  null 0 610.  1  -1.  *hl3 temp
506 time   0          gt  null 0 1.e6  n  -1.  *manual trip
```

In trip 501 the pressurizer pressure is tested against 2300 psia. Trip 502 tests the pressurizer indicated level against the 20% lower limit. It is assumed that control variable 100 has been defined in such a way that a value of 0 corresponds to 0% indicated level and a value of 1 corresponds to 100% indicated level. Trips 503, 504, and 505 test the fluid temperatures in each of the three hot legs against the 610°F upper limit. Trip 506 is a dummy "always false" trip that has been included to provide a convenient method for simulating a manual reactor trip. For example, if a simulation of a reactor trip at 10 seconds is desired, trip 506 would be replaced with

```
506 time 0 gt null 0 10. n -1. *manual trip at 10 sec
```

Next, the variable trips are gathered together into a single trip that is false if none of the variable trips has ever been true and is true if any the variable trips has ever been true:

```
601 501 or 502 1 -1.
602 503 or 504 1 -1.
603 505 or 506 1 -1.
604 601 or 602 1 -1.
605 604 or 603 1 -1. *reactor trip signal
```

With this logic, if any of the variable trips 501 through 506 ever turns true, then trip 605 remains true thereafter. To simulate the 0.5-second delay between the generation of the reactor trip signal and the movement of the scram rods, the status of trip 605 is monitored using a variable trip:

```
507 time 0 gt timeof 605 0.5 1 -1. *scram rod movement
```



## 4.6 Hydrodynamic Components

As a general rule, the user should be cautious of applications where the fluid conditions in the RELAP5 hydrodynamic components may approach the critical pressure. With respect to light water reactor safety issues, this limitation may be of significance to anticipated transient without scram (ATWS) transients. During ATWS events, the reactor is not tripped and continued core power has the potential to drive the primary coolant system pressure upward toward the critical point.

This section discusses specific practices for applying each type of hydrodynamic component. The component type is specified using cards of the format CCC0000 and it is recommended that these cards be the first entered for each component. The inputs required on the remaining cards vary depending on the component type.

### 4.6.1 Single-Volume Component

The single-volume component is the basic hydrodynamic cell unit in RELAP5. Note that the pipe component may be thought of simply as a series collection of single volumes joined by single junctions. A branch component may be thought of as a single volume where one or more single junctions may be combined. The input data specifications describing the basic volume geometries and conditions for the other types of components (pipes, branches, etc.) are identical to those described here for the single-volume component.

The flow area, length, and volume of the cell must be input. As described in the model, these three parameters must be consistent or an input error results. Thus, it is recommended that one of these three quantities be input as zero, allowing the code to calculate its value consistent with the two nonzero entries.

For complex geometries, the requirement that the area, length, and volume be consistent may require the modeler to accept a compromise on one or more of the input parameters. This situation arises when the modeler attempts to include a region with a varying flow area varies within a single hydrodynamic cell.

A compromise is needed because the average flow area for the geometry may not adequately represent the flow path in the region. The input flow area determines the flow velocity, the input length affects the calculated frictional pressure drop, and the input volume contributes to the overall fluid system volume. An additional constraint is that the length input for a vertical cell must be enveloped by the elevation gain of the cell. The modeler should select the compromise that would least affect his particular problem. If the error introduced by all compromises is deemed unacceptable, then more modeling detail should be included by using separate hydrodynamic cells to represent regions with different flow areas.

Azimuth and inclination angles and an elevation change must be input. The azimuth angle input (included in anticipation of a three-dimensional modeling capability) is not currently used by the code; it is recommended that it be entered as 0. An inclination angle from -90 to +90 degrees must be input (note that this entry is always in degrees even if SI units are specific for the problem). An entry of -90 is defined as vertically downward, +90 as vertically upward, and 0

as horizontal. This input is used to select the flow regime map. Volumes whose inclination angles have magnitudes greater than 45° are considered vertical and those whose inclination angles are less than 45° are considered horizontal. Any elevation change specified for a volume must be less than or equal to the maximum allowed using the formula

$$\text{maximum cell elevation change} = \text{cell length} \times \sin(\text{cell inclination angle})$$

An absolute wall roughness and hydraulic diameter must be input. It is recommended that a roughness representing the actual finish of the fluid boundary wall be used. Good modeling results have been obtained using roughnesses of 0.0000457 m (0.00015 ft) for commercial steel finishes and 0.0000015 m (0.000005 ft) for drawn tubing. It is recommended that the classically-calculated hydraulic diameter based on the following formula be used:

$$\text{hydraulic diameter} = 4 \times (\text{flow area}) / (\text{wetted perimeter})$$

For circular geometries (where parallel flow paths have not been lumped together into a single flow path), a zero hydraulic diameter may be input, in which case the code will automatically calculate and use a hydraulic diameter based on the formula

$$\text{hydraulic diameter} = 2 \times (\text{flow area} / \pi)^{0.5}$$

The volume control flags of the format "pvbfe" must be input for each hydrodynamic cell. These flags define the operative code options for each cell. When default flags (00000) are assumed, the water packing is active ( $p = 0$ ), the vertical stratification model is used in volumes that are vertical ( $v = 0$ ), the normal pipe interphase friction model is used ( $b = 0$ ), the wall friction model is active ( $f = 0$ ), and phasic nonequilibrium is allowed ( $e = 0$ ). The default volume control flag options are generally recommended and users should carefully consider the effects of using non-default flags. Guidance for these considerations is provided in Section 3.3.1.

An initial condition control word and corresponding initial fluid conditions are required input for each hydrodynamic cell. For most light water reactor applications, users will find it most convenient to specify initial conditions using control word 3 (pressure and fluid temperature) in subcooled regions and control word 2 (pressure and quality) in saturated regions. A discussion of the other options is provided in Section 3.3.3.1.

Note that each hydrodynamic volume has an inlet and an outlet face that will be used to connect normal junctions to the volume. The inlet and outlet faces are defined as a part of the junction specifications; however, the definition of the faces must be consistent with the elevation change specified. To illustrate, for a volume with a positive elevation change, the lower end of the cell is considered its inlet face and the upper end of the cell is considered its outlet face.

#### 4.6.2 Time-Dependent Volume Component

The TMDPVOL component allows the user to impose a volume-related boundary condition on a model. The term "volume-related" means the condition is one that is normally input as a part of a volume specification rather than a junction specification. For example, pressure, liquid temperature, vapor temperature, void fraction, and quality are volume-related quantities.

For light water reactor modeling, TMDPVOLs typically are employed in two types of applications. First, TMDPVOLs may be used to specify pressure boundaries, generally at locations where fluid exits a model. For example, a TMDPVOL may be used to control the pressure at the inlet of a turbine. The pressure solution throughout the secondary system is then determined by the turbine inlet pressure, the system flow losses, and the system flow rate. When used to specify a pressure boundary, the TMDPVOL is coupled to the remainder of the model using a normal type of junction (such as a single junction or valve). When used in this way, the TMDPVOL actively interacts with the rest of the model.

Second, TMDPVOLs are used to specify fluid conditions at injection sites. For example, a TMDPVOL may be used to specify the temperature of emergency core cooling fluid. When used to specify the fluid conditions at an injection boundary, the TMDPVOL typically is connected to the remainder of the model through a TMDPJUN that effectively isolates the fluid conditions in the TMDPVOL from the remainder of the model. In this application, the TMDPVOL is used simply to provide the proper fluid conditions for an injection flow boundary condition as defined by the TMDPJUN. A discussion of boundary condition specifications is found in Section 3.3.4.

The term "time-dependent volume" is inaccurate; originally, fluid conditions could be specified only as a function of problem time. Current capabilities include specifying the fluid condition in any manner and as a function of virtually any problem variable the user desires.

The boundary condition information entered includes a fluid condition control word, a trip number, a two-word search variable, and a table. The control word defines the variables used to define the fluid state; this option is the same as that described in Section 4.6.1 for the single-volume component. The trip number determines at what problem time the table is to be referenced. The search variable is the code-calculated parameter assumed to be the independent variable of the time-dependent volume table. The dependent entries in the table are the hydrodynamic conditions required to define the fluid state.

As a simple example, consider a time-dependent volume that is to represent a constant pressure atmospheric containment boundary condition for a LCA simulation. Assume that no reverse flow from the containment to the coolant system is anticipated, such as would be the case for a small break. For this purpose, TMDPVOL 580 may be input as follows:

```
*hydro      name      type
5800000     "contain" tmdpvol
*hydro      area      length  volume  horiz  vert  elev  rough  dh  flags
5800101     1.e6      0.      1.e6    0.     0.     0.     0.     0.  00010
*hydro      ebt       trip     alphacode  numericcode
5800200     3
*hydro      time      pressure  temp
5800201     0.        14.7     213.
```

The data input on card 5800101 are virtually immaterial to the problem since the TMDPVOL is being used only to define the pressure condition. Control word 3 specifies that the table should indicate the boundary conditions for pressure and fluid temperature. Since a constant pressure condition is desired, only one entry is needed in the table: time 0., 14.7 psia,

212°F. Note that since no reverse flow is anticipated, the fluid temperature specified is also immaterial. At 14.7 psia, a temperature of 213°F is a superheated vapor. However, in this application, the problem solution would be identical even if a subcooled liquid state was specified.

Now consider that it is desired to include the effects of a variable containment pressure during the calculation. Assume it is known that for this accident the break flow will pressurize the containment linearly from 14.7 psia to 50 psia over 15 seconds and that the containment coolers will then reduce the pressure to 20 psia over another 10 seconds. This effect could be included in the above example by entering a table that reflects this pressure response:

```
*hydro  time  pressure  temp
5800201  9.    14.7    213.
5800202  15.   50.    213.
5800203  25.   20.    213.
```

The boundary condition may be tailored to any particular specification by employing and combining the trip and search variable options. The trip option allows the user to implement the table at any problem time, or as a result of any occurrence in the calculation, as desired. By specifying a search variable other than time, the boundary condition may be made a function of any calculated parameter.

To illustrate, consider extending the above example in the following way. Assume the break is to open when the pressurizer level falls below 20%. The break will be modeled using a trip valve component and say that trip 510 is used to compare a control variable representing the pressurizer level against the 20% limit. Because it is not known in advance at what time the coolant pipe break into containment will occur, trip 510 will also be used to trip the TMDPVOL parameter table. Further assume that the containment pressure response is known as a function of the integrated break flow. Elsewhere, control variable 105 is used to calculate the integrated break flow. To model this situation, the time-dependent volume input might appear as follows:

```
*hydro  name  type
5800000  "contain"  tmdpvol
*hydro  area  length  volume  horiz  vert  elev  rough  dh  flags
5800101  1.e6  0.    1.e6  0.    0.    0.    0.    0.  00010
*hydro  ebt   trip   alphacode  numericcode
5800200  3     510   cntrlvar  105
*hydro  cntrlvar  105  pressure  temp
5800201  -1.e99  14.7  213.
5800202  0.     14.7  213.
5800203  1.     16.   213.
5800204  10.    20.   213.
5800205  150.   30.   213.
5800206  500.   35.   213.
5800207  1000.  36.   213.
```

With this format, the status of trip 510 is monitored. As long as the trip is false, the table returns a pressure of 14.7 psia (as indicated by the pressure associated with the -1.e99 independent

variable). After the break opens and trip 510 turns true, the containment pressure is determined as the pressure in the table corresponding to the current value of the integrated break flow (control variable 105).

An initialization problem with TMDPVOLs can be encountered if a search variable from a higher-numbered component is specified. The components are initialized in numerical order. Therefore, if a TMDPVOL uses a condition (pressure, temperature, etc.) from a higher-numbered component, an indeterminate condition is reached because that component has not yet been initialized. This problem can be circumvented by always referencing lower-numbered components or by referencing a control variable (such as in the above example) that has been initialized by the user.

### 4.6.3 Single-Junction Component

The single junction is the basic hydrodynamic flow unit in RELAP5. The input data specifications describing the basic junction properties and conditions for the junctions associated with other types of components (pipes, branches, etc.) are identical to those now described for the single-junction component.

The "from" and "to" components must be specified for each junction. As discussed in Section 4.6.1, each component has an implied inlet and outlet face. The "from" and "to" component callouts for junctions refer to the component number, a two-digit face identifier, and four trailing zeros. When connecting to a component's inlet face, the appended digits are 00. When connecting to a component's outlet face, the appended digits are 01. For example, consider a junction that connects the outlet of pipe 150 to the inlet of single volume 160. The "from" code entered is 150010000 and the "to" code entered is 160000000.

The "from" and "to" identifiers specify the direction of positive junction flow. In the above example, flow from component 150 to component 160 will be considered positive by the code; flow in the opposite direction will be considered negative.

It is necessary to input a junction flow area. If zero is input, then the code assumes that the junction area is the minimum flow area of the adjacent hydrodynamic volumes. It is also required to input forward and reverse loss coefficients (although zeros may be specified). This input allows the user to insert flow losses associated with irregular pipe geometries such as are found at bends and fittings. The total flow loss will be based on a combination of losses from interphase drag, wall friction, abrupt area change, and user-specified loss coefficients. All loss coefficients are referenced to the user-input junction area (or that calculated by the code as explained above).

It is also necessary to enter the "fvcahs" junction control flags and initial velocity or flow conditions for each junction. Details regarding selection of the junction flags are described in Section 3.3.2 and details regarding initial condition input are described in Section 3.3.3.2.

Regarding the selection of the abrupt or smooth area change model at junctions, the abrupt area change option may be used to represent the flow losses through sudden contractions and expansions. When selected, the code calculates the loss based on the area change ratio and the current fluid conditions. It is recommended that this option not be used in situations where the



area change ratio is greater than 10. For this situation, the smooth area change option and an appropriate loss coefficient is recommended.

Regarding the selection of the choking flag, recent user experience with very low pressure applications (near atmospheric, and at vacuum conditions) has indicated the RELAP5 choking model may be inadequate at low pressures. In these applications, the choking model has generally been disabled (by specifying  $c = 1$ ). However, for more traditional applications it is recommended that the choking model generally be used (by specifying  $c = 0$ ).

The optional countercurrent flow limiting (CCFL) data card is available for input at junctions. The use of the CCFL model is discussed in Section 3.4.6. While this card is termed optional, the junction hydraulic diameter is specified on the card. If the card is not input, then a default junction hydraulic diameter, based on a circular junction flow area, is used. For noncircular geometries, and for "lumped-loop" situations, the code-calculated default junction hydraulic diameter will not be correct. The junction hydraulic diameter is used in the formulation of interphase drag for all junctions, not just at junctions where the CCFL model has been implemented. The word optional on the CCFL data card therefore should be interpreted "required for all junctions where the default hydraulic diameter is not acceptable or the CCFL model is to be implemented."

#### 4.6.4 Time-Dependent Junction Component

The TMDPJUN component permits the user to impose a flow boundary condition on a model. It is possible to specify the flow condition as either a volumetric or mass flow rate. An illustrative example of this capability is the specification of an injection flow as a function of the coolant system pressure (e.g., for the flow delivered from an ECC system employing centrifugal pumps).

As is the case for a TMDPVOL component described in Section 4.6.2, the TMDPJUN specifies a trip number, a search variable, and a table that correlates the search variable to the flow boundary condition. To model the ECC system described above, the TMDPJUN input might look as follows:

*hydro	name	type			
5900000	"eccs"	tmdpjun			
*hydro	from	to	area		
5900101	585000000	595000000	0.05		
*hydro	vel/flow	trip	alphanumeric	numeric	
5900200	1	575	p	595010000	
*hydro	p	mdot-l	mdot-v	mdot-if	
5900201	-1.e99	0.	0.	0.	
5900202	0.	0.	0.	0.	
5900203	500.	250.	0.	0.	
5900204	1000.	200.	0.	0.	
5900205	1500.	120.	0.	0.	
5900206	2000.	60.	0.	0.	

5900207	2400.	25.	0.	0.
5900208	2500.	0.	0.	0.

Assume that trip 575 has been defined as the safety injection actuation signal and no ECC flow is possible until certain conditions are met. Before the status of this trip turns true, no flow will be injected by TMDPJUN 590 (when the trip is false the flow associated with a negative search argument is used). After the trip turns true, a search is made in the table using the pressure in cell 59501 to evaluate the injection flow mass flow rate. With the input shown above, the shutoff head of the injection pump is 2500 psia and as the pressure falls, the injection flow rate increases in a manner prescribed in the table. Component 585 would be modeled with a TMDPVOL that specifies the temperature of the injection fluid.

#### 4.6.5 Pipe/Annulus Component

The pipe component is simply a series combination of single-volume and single-junction components. Component descriptions and input requirements are presented in Section 4.6.1 for the single-volume component and in Section 4.6.3 for the single-junction component. The advantage of the pipe over the separate single components is primarily one of input efficiency. For example, the number of data cards needed to input a ten-cell pipe is significantly fewer than to input the corresponding ten single volumes and nine single junctions. This efficiency results from using the sequential expansion input format.

As an example of the sequential expansion format, consider the input needed to specify the flow areas for a seven-cell pipe. For the first two cells, the flow area is 1 ft<sup>2</sup>, for the third cell it is 4 ft<sup>2</sup>, and for cells 5, 6, and 7, it is 2 ft<sup>2</sup>. These data are entered for component CCC as follows:

```
CCC0101 1. 2. 4. 3. 2. 7.
```

This data is read by the code as 1 ft<sup>2</sup> through Cell 2, 4 ft<sup>2</sup> through Cell 3, and 2 ft<sup>2</sup> through Cell 7.

By definition, the pipe component has only internal junctions associated with it. Any connections to the ends of a pipe must be made with external junctions (e.g., single junctions, valves, time dependent junctions, or junctions associated with branch-type components). RELAP5/MOD3 includes a new capability to connect external junctions to internal pipe cells. To exercise this capability, it is necessary to use the expanded connection code option of RELAP5/MOD3 [see the description of the single-junction component in the user input manual (Carlson et al., 1990a)].

Flow branching may be accomplished by connecting two or more external junctions at the end of a pipe component; it is not necessary to use a branch component for this purpose. A non-fatal warning message will appear in the printed output indicating that more than one junction is attached at a pipe end.

The annulus component is identical to the pipe component except that an annular flow regime map is used. An annulus must be specified as a vertical component.

#### 4.6.6 Branch Components

The branch component may be thought of as a single-volume component that may have single junctions appended. Component descriptions and input requirements are presented in Section 4.6.1 for the single-volume component and in Section 4.6.3 for the single-junction component.

Any number of junctions may be defined as a part of a branch component. Note that other external junctions (e.g., single junctions, valves, and time dependent junctions) that are defined separately may also connect to a branch.

The separator, jet-mixer, turbine, and ECC-mixer components are specialized branch components. Certain restrictions on the number and orientation of junctions apply for these specialized components. Brief discussions regarding use of these specialized branches are presented in the following subsections.

**4.6.6.1 Separator.** The separator component is a specialized branch mainly used for simulating the behavior of light water reactor steam separators. Three junctions must be defined with a separator and no junctions defined in other components may connect to a separator. By definition, junction 1 must be the vapor outlet junction, junction 2 must be the liquid return junction, and junction 3 must be the separator inlet. Recommendations and restrictions for separator user option selection are documented in Section A-7.7 of the RELAP5 user input data requirements manual (Carlson et al., 1990a).

The separator component accepts the inlet flow, performs an idealized prescribed separation of the liquid and vapor phases, and when in the separating mode passes the vapor out the separator outlet junction and passes the liquid out the liquid return junction. Example nodalizations of separator applications are documented in Section 5.

The separation process is directed by the void fraction limits associated with the last entries on the input cards for the vapor and liquid outlet junctions. For the vapor outlet junction, this entry is termed VOVER and represents the *vapor fraction* above which the outlet flow is pure vapor. For the liquid return junction, this entry is termed VUNDER and represents the *liquid fraction* above which the flow out the liquid return junction is pure liquid.

The VOVER and VUNDER limits are based on the separator hydrodynamic cell conditions, not the junction conditions. For void fractions greater than VOVER and less than  $(1 - \text{VUNDER})$  an idealized separation process is used. This idealized process involves a total separation of the fluid entering the separator inlet junction. Pure vapor passes through the outlet junction and pure liquid is returned through the liquid return junction. For void fractions less than VOVER, the separator is assumed to be flooded and liquid may flow out the vapor outlet junction. For void fractions greater than  $(1 - \text{VUNDER})$  the separator is assumed to be drained and vapor may be carried under through the liquid return junction. When outside the range of void fractions for the idealized separation mode, the separator component reverts to the normal branch component models.

Default values of  $VOVER = 0.5$  and  $VUNDER = 0.15$  are used if not specified by the user. With these values, an idealized separator is modeled when the void fraction is between 0.50 and 0.85. The user must therefore ensure that the separator void fraction is between the limits specified when simulating a normal separator operation. Separator performance in off-normal situations is an area of considerable uncertainty. There is a general lack of available separator test data that may be used to correlate appropriate liquid carryover and vapor carryunder limits (Westinghouse Electric Co. et al., 1987)

**4.6.6.2 Jet-mixer.** The jet-mixer component is a specialized branch that is mainly used for simulating the behavior BWR jet pumps. Three junctions must be defined and no junctions defined in other components may connect to a jet-mixer. By definition, junction 1 must be the drive, junction 2 must be the suction, and junction 3 must be the discharge. Recommendations and restrictions for jet-mixer user option selection are documented in Section A-7.7 of the RELAP5 user input data requirements manual (Carlson et al., 1990a).

The jet-mixer uses the momentum of the drive junction to accelerate the suction flow through the discharge junction. There has been only limited user experience applying the jet-mixer component. Example nodalizations of jet-mixer applications are documented in Section 5.

**4.6.6.3 Turbine.** The turbine component is a specialized branch that allows for work extraction. A simple turbine may be modeled using one turbine component; multistage turbines may be modeled using a series combination of turbine components. Each turbine component must define two junctions. Junction 1 must be the inlet junction and Junction 2 must be a crossflow junction for steam extraction. The normal turbine outlet junction must be defined as a part of another component (such as a single-volume or branch). Recommendations and restrictions for turbine user option selection are documented in Section A-7.7 of the RELAP5 user input data requirements manual (Carlson et al., 1990a).

The turbine component requires additional input data requirements (beyond those for a branch) to define rotor geometry and performance parameters. A turbine component may be connected to a control variable shaft component, which in turn may be connected to a control variable generator component. With this arrangement, the speeds, loads, and inertias of the turbine, shaft, and generator are determined consistently.

There has been no user experience applying the turbine component beyond that in code developmental assessment. The turbine component has never been used successfully in a steam/water system. However, there has been a successful steady-state application of the turbine model using hydrogen as a working fluid. In that application, a simple single-stage turbine was used. There has been no experience with multiple-stage turbines; it is recommended that a single-stage turbine be modeled unless bleed paths are needed from each stage. In the successful application, turbine type 2 was used; a reaction fraction and stage radius are not used when this option is selected. In this application, the turbine power extracted was found to be entirely dependent on the differential pressure across the turbine. Other parameters had virtually no effect.

**4.6.6.4 Emergency Core Cooling Mixer.** The ECC-mixer component is a specialized branch that may be used to simulate the phenomena associated with subcooled ECC injection into

a reactor coolant system. The ECC-mixer component is a new model that has not existed prior to RELAP5/MOD3 so user experience is restricted to developmental assessment applications. The purpose of the model is to provide a more representative simulation of the flow regimes and interphase heat transfer processes associated with a subcooled liquid stream entering a voided pipe.

The ECC-mixer component should be centered at the injection site and preferably have a length-to-diameter ratio greater than 3. It is necessary to specify three junctions. Junction 1 is the injection junction, junction 2 is the normal inlet, and junction 3 is the normal outlet. Recommendations and restrictions for ECC-mixer user option selection are documented in Section A-7.7 of the RELAP5 user input data requirements manual (Carlson et al., 1990a). Note that the user may specify an injection angle by using the last word on the data input card describing junction.

#### 4.6.7 Valve Component

The valve component provides a general capability for specifying a junction with a variable flow area. The input requirements for the single-junction component described in Section 4.6.3 also apply to the valve component. A restriction prevents a valve from being used as a crossflow junction, but they may be used in all applications where a single-junction component may be used.

A valve type must be specified. This selection is dictated by the manner in which the user would prefer the valve to be controlled. Available valve types include check, trip, inertial, motor, servo, and relief. Recommendations and restrictions for valve user option selection are documented by valve type in Section A-7.8.5 of the RELAP5 user input data requirements manual (Carlson et al., 1990a). Descriptions and example applications for each valve type are presented in the following subsections. For light water reactor safety applications, the check, trip, and servo valves are particularly useful, the motor valve is moderately useful, and the inertial and relief valve components are not recommended. Because code assessments have highlighted the importance of adequately modeling actual valve performance, it is recommended that the user carefully consider the modeling of valves. Factors such as valve closure time, closing characteristics, and leakage have been shown to significantly affect simulations.

**4.6.7.1 Check Valve.** The check valve component is used as a flow control device to prevent back flow of fluid from one region into another when the downstream pressure is higher than the upstream pressure. Check valves are employed at many locations in a light water reactor. Examples include ECC injection, accumulator injection, and feedwater injection lines. When modeling a system, check valve components are simply included at the same location as the prototype valves.

It is recommended that the check valve type be specified using option 0. Numerical difficulties have been experienced when using option 1. The check valve component is fully open whenever the upstream pressure exceeds the downstream pressure and fully closed whenever the reverse is true. Check valves generally have been applied using zero closing back pressures and leak ratios. User experience has shown that, when leakage is to be modeled, the valve must have been open previously for the leakage to be simulated. To simulate leakage with a check valve



that should always be closed, initialize the valve open and let local pressures close it immediately when the calculation begins.

**4.6.7.2 Trip Valve.** The trip valve component is used whenever a binary control (i.e., open or closed) valve is needed. The binary operator used is the trip (described in Section 4.4). The trip valve is fully open whenever its associated trip is true and fully closed whenever its associated trip is false. Since control logic for many prototype valves may be reduced to a binary operation, the trip valve is used frequently. Example applications for a trip valve include isolation valves and relief valves. An accumulator system might contain an isolation valve that must be opened to allow flow or closed when the tank has emptied. A relief valve might be open if certain conditions are present and closed if not. Example 2 in Section 4.4.2 illustrates how the behavior of a hysteresis relief valve may be simulated with trip logic.

The trip valve is also valuable in providing modeling flexibility. For example, consider a study to find the sensitivity of calculated results to various flow systems. The modeler may include all flow systems in a base model and will then have the capability to "valve-out" flow systems by employing isolating trip valves. The sensitivity calculations may proceed using the same model. The appropriate flow systems are selected by altering trip status as needed.

**4.6.7.3 Inertial Valve.** The inertial valve allows the user to simulate the detailed response of a check valve based on the hydrodynamic forces on the valve flapper and its inertia, momentum, and angular acceleration. Unless the dynamic response of the valve itself is of particular importance to a problem, it is recommended that the inertial valve not be used. The check valve component described in Section 4.6.7.1 is recommended for that purpose. There has been only limited user experience applying the inertial valve component.

**4.6.7.4 Motor Valve.** The motor valve component lets the modeler simulate a valve that is driven open or closed at a given rate following the generation of an open or close command. Trip status is used to generate the open and close commands; one trip number is identified as the open trip and another as the close trip. The valve responds by maintaining its current position unless either the open or close trip is true. When opening or closing, the valve area is reduced at a specified change rate. The change rate is specified as a time constant in units of inverse seconds. A change rate of 0.1 therefore indicates the valve area changes from full closed to full open (or the reverse) in 10 seconds.

The model also allows the user to incorporate a nonlinear valve area response. If a valve table number is identified, the table is assumed to correlate the valve stem position and the valve flow area. In the above example, the stem position would be assumed to vary from 0 to 1 (or 1 to 0) over 10 seconds. A nonlinear valve flow area response may then be incorporated through the valve table.

The motor valve would appear to be very useful, but the need to specify a constant change rate limits its applicability. Generally, it is recommended that a motor valve component be used only in applications where the valve change rate in the prototype system is well known and where realistic simulation of this valve control is important to the problem. For most applications, the servo valve is a more appropriate selection because of greater flexibility in its control.

**4.6.7.5 Servo Valve.** The servo valve component is the most flexible valve model. Its normalized flow area is equal to the current value of a specified control variable. For a control variable value of 0, the valve is fully closed and for a value of 1 it is fully open. Thus, virtually any process, accessing virtually any calculated parameter, may be reduced through control variable logic to a normalized flow area and used to control the valve position.

As for the motor valve, the user can incorporate a nonlinear valve area response. If a valve table number is identified, the table is assumed to correlate the valve stem position and the valve flow area. In this case, the specified control variable is interpreted as the normalized stem position and a nonlinear valve flow area response may then be incorporated through the valve table.

To demonstrate the power of the servo valve component, consider modeling a prototype feedwater control system for a PWR with U-tube steam generators. The feedwater flow rate is controlled by modulating the feedwater valves based on the response of a three-point control system. The feedwater flow rate, steam flow rate, and steam generator indicated level are measured and used to drive a complex control system. This system processes the feed/steam flow mismatch and level errors through proportional-integral controllers into a valve movement command. If this control system is accurately modeled using the RELAP5 control variable logic described in Section 4.10, then the modeled control system output may be arranged such that a control variable will represent the normalized feedwater valve flow area. The feedwater valve is then modeled using a servo valve component that references that control variable.

**4.6.7.6 Relief Valve.** The relief valve gives the capability to simulate the detailed response of a spring-loaded relief valve based on the hydrodynamic forces on the valve pintle, and its mass, momentum, and acceleration. Unless the dynamic response of the valve itself is of particular importance to a problem, it is recommended that the relief valve not be used. The trip valve component described in Section 4.6.7.2 and the trip logic described in Section 4.4.2 Example 2 are recommended for that purpose. There has been only limited user experience applying the relief valve component.

#### 4.6.8 Pump Component

The input and performance of the pump component is arguably the most misunderstood of the RELAP5 models. The pump component consists of a single hydrodynamic volume with appended inlet and outlet junctions. By definition, junction 1 is the pump inlet and junction 2 is the outlet junction. The pump model acts simply as a momentum source that produces a pump differential pressure with a corresponding pump head. The pump head is apportioned equally between the inlet and outlet sides. In other words, the pump center pressure is midway between the inlet and outlet pressures.

The pump head is calculated based on the rated pump conditions, a normalized set of pump characteristics (the homologous curves), and the currently-calculated conditions (e.g., pressure, temperature, void fraction, and flow rate). Because the pump performance is explicit, the solution is based on the conditions present in the previous time step. Therefore, the user should check for stability difficulties with the pump model that may be encountered when (a) the time step size is

large, (b) the calculated phenomena are changing rapidly, or (c) the slopes of the homologous curves are particularly steep.

The homologous curves are wide single-phase performance relationships between the pump flow, head, and speed. These relationships are non-dimensionalized using the pump rated conditions. If needed, the pump model provides the capability to degrade the pump performance as a function of the coolant void fraction in the pump.

**4.6.8.1 General Pump Input.** Much of the input required for the pump component is similar to that presented for the single-volume and single-junction components described previously and will not be repeated here. The reader is urged to read the input requirements section of the code manual for several input restrictions (Carlson et al., 1990a). Some general model options are not available for the pump component. The most commonly encountered restriction is that heat structures may not be connected to a pump hydrodynamic volume.

The CCC0301 card (CCC is the component number) is used to input the flags that specify the locations of the pump data, the two-phase and motor options, and the pump speed control, the pump trip number, and whether reverse pump speeds are allowed.

The CCC0302-04 cards are used to input the pump rated conditions and other pump parameters. In general, the pump rated conditions are available in data supplied by pump manufacturers. Note that the pump rated speed and ratio of initial to rated speeds are input. The pump does not need to be initialized at its rated speed. Input for the moment of inertia should include all rotating masses: pump, shaft, and motor. The friction torque inputs (TF0, TF1, TF2, and TF3) are used to model the bearing friction drag for the pump. The friction torque is determined from the cubic equation:

$$\text{friction torque} = \text{TF0} + \text{TF1} \times S + \text{TF2} \times S^2 + \text{TF3} \times S^3$$

where

$S$  = the ratio of current speed to rated speed.

This input allows the bearing friction torque to be specified as a function of pump speed. The rated speed, flow, head, torque, density, and motor torque are used along with homologous curves to calculate pump performance when the pump is powered. Following a pump trip, pump coastdown will be determined by the moment of inertia, the friction torque, and the interaction (through the homologous curves) between the pumped fluid and the impeller. It is recommended that the user input a nonzero friction torque because if it is specified as zero the pump speed coastdown following trip may not end at zero speed. In other words, if the rotor is considered to be frictionless, then it will tend to "pinwheel" in any residual flow, such as from natural loop circulation. This effect can be important because the locked-rotor pump resistance is a significant portion of the overall loop resistance at natural circulation flow rates. The difference between locked-rotor and pinwheeling resistances is considerable. As a starting point, it is recommended that a total of 2% of rated torque be used as friction torque. Furthermore, it is recommended that this 2% be evenly divided between torques TF0 and TF2; therefore, 1% represents static bearing friction and 1% represents bearing friction proportional to the square of the pump speed.

**4.6.8.2 Homologous Curve Development.** The RELAP5 homologous curves provide the data needed for the code to calculate single-phase pump performance. RELAP5 contains built-in homologous curves for a Westinghouse and a Bingham-Willamette pump. To avoid considerable extra effort, the pump to be modeled should be represented with one of the built-in options if possible. Homologous curve selection is made using the first field on card CCC0301: 0 indicates the curves are to be input, a positive number indicates the curves input for the component with the same number are to be used, -1 indicates the Bingham-Willamette curves are to be used, and -2 indicates the Westinghouse curves are to be used.

If the user determines that homologous curves need to be input, then the data for a full set of curves must be developed. The nature and terminology of the homologous curves are somewhat unique in the development of thermal-hydraulic systems models. Therefore, curve development therefore is often a source of confusion for the model developer. The remainder of this section is intended to reduce this confusion by explaining the terminology and the development process.

Two sets of pump homologous curves provide the relationships among head, flow, and speed (termed the head curves) and among torque, flow, and speed (termed the torque curves). These curves are non-dimensionalized by the rated head, rated torque, rated flow, and rated speed specified for the pump. Next, the curves are expressed in terms of unique independent variables (the ratio of normalized flow to normalized speed).

Four modes of pump behavior are possible: normal pump, energy dissipation, normal turbine, and reverse pump. These modes are summarized in Table 4-1. Because the curves are normalized, two regions are needed for each of these modes to describe either the head or torque curves: one for when the independent variable ranges from 0.0 to 1.0 and one when the independent variable is greater than 1.0. In this latter case, the independent variable is inverted.

**Table 4-1.** Modes of pump operation.

<u>Mode</u>	<u>Characteristics</u>
Normal pump	Positive flow and positive speed
Energy dissipation	Negative flow and positive speed
Normal turbine	Negative flow and negative speed
Reverse pump	Positive flow and negative speed

Because of this inversion, the homologous curves can compress the entire range of pump performance between independent variable values of -1.0 and 1.0. A full set of homologous head curves contains eight regimes (two each for the normal pump, energy dissipation, normal turbine, and reverse pump modes). Similarly, a full set of homologous torque curves also contains eight regimes. It is a requirement that input be provided for all sixteen head and torque regimes.

Figure 4-1 shows an example set of homologous head curves with the standard regimes indicated. Note that the regimes and modes correspond with each other: regimes 1 and 2 to the normal pump mode, regimes 3 and 4 to the energy dissipation mode, regimes 5 and 6 to the normal turbine mode, and regimes 7 and 8 to the reverse pump mode. The normalized independent and dependent variables are defined in terms of the head, flow, and speed ratios as shown in the figure. A similar set of eight regimes is needed for the homologous torque curves. For these, the head ratio is replaced by the comparable torque ratio.

Generally, pump test data are available for the normal pump mode. Typical pump test curves provide head as a function of flow at a constant speed and this data is sufficient to generate the head homologous curves for regimes 1 and 2. This is accomplished by tabulating the pump test data for flow and head, normalizing the data based on the rated conditions, and calculating the requisite nondimensional independent and dependent variables shown in Figure 4-1. The torque homologous curves for regimes 1 and 2 may be calculated by extending the tabulation from the head curve calculation and considering that the normalized torque is equal to the product of the normalized flow and normalized head divided by the normalized efficiency.

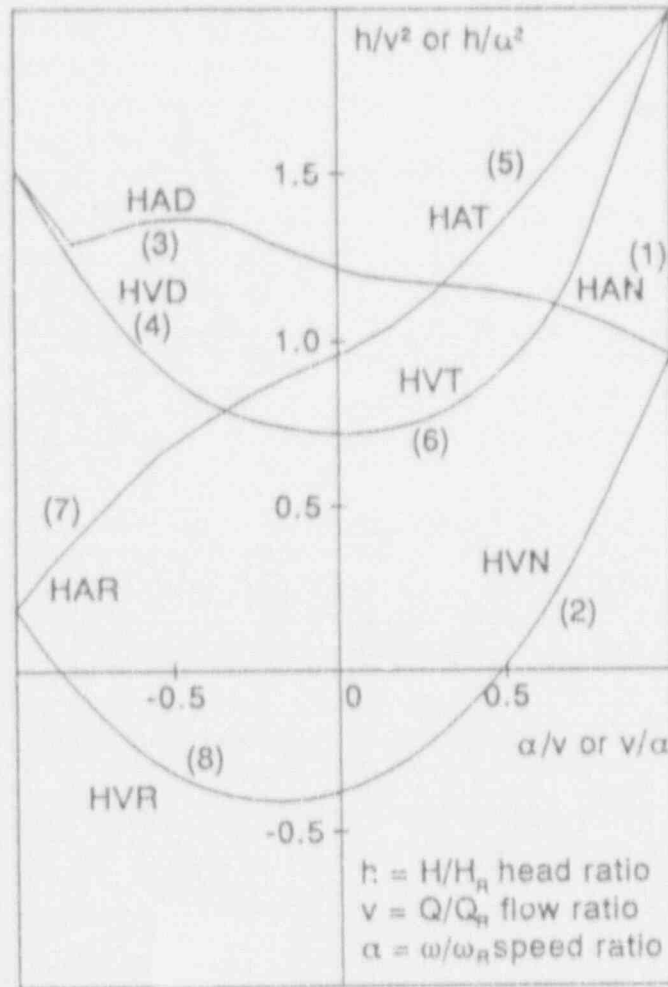
Pump test data supporting development of the head and torque curves for regimes 3 through 8 are generally unavailable. It is suggested that a user with no other option consider using data similar to that shown in Figure 4-1 for regimes 3 through 8 as a means of obtaining reasonable responses in the off-normal regimes. It is important that the regime curves form a closed pattern, such as is shown in Figure 4-1. Regime intersection points are summarized in Table 4-2. An open pattern will result in grossly-inappropriate pump model performance or job

**Table 4-2.** Homologous curve regime consistency requirements.

<u>Curves</u>	<u>Independent Variable</u>
1 and 2	1.0
1 and 3	0.0
2 and 8	0.0
4 and 3	-1.0
4 and 6	0.0
5 and 6	1.0
5 and 7	0.0
7 and 8	-1.0



Normal pump	(+Q, +α)	{ HAN HVN
Energy dissipation	(-Q, +α)	{ HAD HVD
Normal turbine	(-Q, -α)	{ HAT HVT
Reverse pump	(+Q, -α)	{ HAR HVR



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Figure 4-1. Single-phase homologous head curves for 1½ loop MOD1 semiscale pumps.

failure whenever a transition is attempted from one curve regime to another across a discontinuity.

**4.6.8.3 Pump Two-Phase Degradation Characteristics.** The two-phase degradation of pump performance is specified using difference and multiplier curves. The degraded pump head is calculated by subtracting the product of the head multiplier and the single-phase/two-phase difference head curves from the single-phase head curves. A similar method is used to calculate the degraded torque. Formulas for these relationships are found in the code manual (Carlson et al., 1990b). Note that the multiplier curves are specified as functions of pump void fraction and that the multipliers should equal 0.0 at void fractions of 0.0 and 1.0.

Unfortunately for the code user, the data needed to develop the two-phase difference and multiplier input often are not available. As is the case for the off-normal, single-phase pump, homologous curve regions described in Section 4.6.8.2, pump manufacturer test data neglect many of the pump operating regimes needed to fully characterize pump behavior. Two-phase difference and multiplier data for a semiscale pump are available and are documented in the code manual (Carlson et al., 1990b); however, no assurances can be given regarding its use in other applications.

The two-phase pump performance degradation model is based on the pump-center void fraction. This can be the cause of anomalies if the void fraction data on which the degradation behavior is based were taken at the pump inlet. The difference between pump inlet and center void fractions can be especially significant for highly voided inlet conditions at very low pressures. As the fluid passes into the pump, the voids are compressed and the pump center void fraction may be much lower than that at the pump inlet. If this is expected to be an important effect, then the user may modify the input to account for it. This modification is made by specifying the multiplier curves as functions of pump-center void fractions that have been adjusted to reflect the differences between pump entrance and center conditions.

The user should note that the RELAP5 pump does not contain a cavitation model. The two-phase degradation behavior discussed above regards voiding within the pump hydrodynamic cell based on convection of void from upstream cells or bulk flashing within the pump itself. A mechanistic model of flow on the pump impeller is not included. If the user finds that pump cavitation effects are to be expected and data regarding pump performance during cavitation are available, then an approximation of cavitation behavior may be implemented independently. This implementation involves monitoring conditions using RELAP5 control variables and, where appropriate based on the data, reducing the pump speed to simulate cavitation effects.

**4.6.8.4 Pump Speed Control.** Control of the RELAP5 pump model speed is a frequent source of confusion to users. The pump simply has two modes of operation, untripped and tripped. In the untripped mode, the pump speed may be controlled by the user in any manner desired. For example, a constant pump speed may be specified, or the pump speed may be controlled as any function of other problem variables via a RELAP5 control variable. In the tripped mode, the user may not control the pump speed. It is determined by the dynamics of the pump rotating masses and interaction between the pump and its fluid through the homologous curves. In a typical application, a pump's speed may be controlled as a constant until some pump

trip condition is met (e.g., attaining a low system pressure). Following trip, the pump coasts down to zero speed.

The trip condition of the pump is determined by two trips. The first trip is contained on card CCC0301, where CCC is the pump component number. When this first trip is false, the pump is considered to be untripped, and when it is true, the pump is considered to be tripped. The second trip is found on card CCC6100. When this second trip is false, the pump is considered to be tripped and when it is true, the pump is considered to be untripped. Furthermore, the status of the second trip overrides that of the first trip, and if the second trip is specified as 0 then the condition of the second trip is assumed to always be true. To avoid confusion, it is recommended that the first and second trips be specified as complementary trips. In this manner, there is no doubt to the user whether or not the pump is tripped.

For an untripped pump, its speed is determined by the time-dependent pump velocity control cards and table on cards CCC6100, CCC6101, etc. The term "time-dependent" is inaccurate. These cards provide the flexibility to specify the pump speed as a function of any calculated parameter.

For a tripped pump, RELAP5 calculates its speed response based on an inertial coastdown from its condition at the time of trip and the hydrodynamic interaction between pump and fluid based on the pump homologous curves. The user is referred to Section 4.6.8.1 regarding the importance of specifying realistic pump-bearing friction so that under normal circumstances pump coastdown will result in a locked rotor.

To illustrate pump speed control, consider an example of trying to control the speed of pump 135 as a function of the pressure in hydrodynamic cell 340010000. This example might represent a turbine-driven pump whose speed is known as a function of the pressure available to drive the turbine. In addition, assume that when the pressure in cell 340010000 falls below 50 psia that the turbine and pump are tripped and coast down. First, the two pump trips are developed:

```
535 P 340010000 LT NULL 0 50. L -1.  
635 -535 AND -535 N 0.
```

Trip 535 is initiated as false and will latch true when the pressure falls below 50 psia. Trip 635 is specified as the complement of trip 535 and therefore is initiated as true and will remain true until it is latched false when trip 535 turns true. Trip 535 will be used as the trip on card 1350301 and trip 635 will be used in the speed table that will appear as follows:

1356100	635	P 340010000
1356101	0.	0.
1356102	50.	27.
1356103	300.	125.
1356104	700.	180.
1356105	1000.	185.
1356106	5000.	185.

The speed table, which correlates pressure and pump speed, therefore is in effect whenever trip 635 remains true. The table uses the pressure in cell 340010000 as the independent search variable. The table dependent variable is the pump speed, in this case in RPM. When trip 635 turns false and trip 535 turns true, speed control switches from the speed table to an inertial coastdown.

Note that the user is not constrained to specifying pump speed in table format as in the above example. The pump speed may be determined in any manner desired using RELAP5 control variables. The control variable and pump speed are then related by a one-to-one correspondence pump speed table. To illustrate, in the above example say that the pump speed is calculated using control variables and that the output of this process is control variable 405, which represents the desired pump speed. Speed control is effected by using a speed table such as

```
1356100 635 CNTRLVAR 405
1356101 0. 0.
1356102 1.e6 1.e6
```

With this method, the pump speed is set equal to the value of control variable 405 by the table.

#### 4.6.9 Multiple-Junction Component

The multiple-junction component is a new model in RELAP5/MOD3 and as such has had little user experience. By using this component, the user can specify many junctions with a single component. This provides an alternative to specifying many independent single-junction components.

The advantages of using the multiple-junction component are that (a) the input required for the junctions is minimized, and (b) data for all junctions may be consolidated in a single location in the input stream. The disadvantage of using the multiple-junction component is that identifying the locations of the junctions in printed and plotted output becomes more difficult.

To illustrate this disadvantage, consider that components may be joined using junctions within the components themselves or with separate junction components. If the components of a flow circuit are numbered consecutively (e.g., 100, 110, 120, 130), then the locations of the junctions are easily identified by the output parameters. In the above example, junction 105 is easily recognized as connecting components 100 and 110 and junction 120010000 is understood to connect to component 120. If, however, a multiple-junction component is used, then all of the junctions associated with it would share the same component number (in the above example, junction 100010000 would connect components 100 and 110, 100020000 would connect 110 and 120, 100030000 would connect 120 and 130, and so on). Identification of the junction locations in the output then becomes problematic.

In the authors' opinion, the disadvantages of using the multiple-junction component outweigh its advantages in most applications. Therefore, it is recommended that use of multiple-junction components generally be avoided.

#### 4.6.10 Accumulator Component

The accumulator component is a lumped parameter component for which special numerical treatment is given. The model provides a realistic calculation of the phenomena associated with tank draining, gas bubble expansion, wall heat transfer, and interphase heat transfer at a quiescent liquid-gas interface. The accumulator therefore lets the user simulate a nitrogen-charged accumulator and surge line system. The accumulator must be initialized with the gas and liquid spaces in thermal equilibrium and with no surge line flow. Note that the accumulator tank, tank wall, surge line, and outlet check valve junction are included in the accumulator model.

During a simulation where an accumulator tank is calculated to drain, the special accumulator models are disabled and the model reverts to a normal single volume hydrodynamic solution scheme. The gas used in the accumulator is assumed to be nitrogen, which must be one of the gas types specified on card 110.

### 4.7 Heat Structures

RELAP5 heat structures are used to represent metal structures such as vessel walls, steam generator tubes, fuel rods, and reactor vessel internals in a facility. Each heat structure is defined to have a "left" side and a "right" side. Conventions such as these are described below. Each side of a heat structure may be connected to at most one hydrodynamic volume. However, more than one heat structure may be connected to the same hydrodynamic volume.

The user should consider that the average fluid conditions in the hydrodynamic volume are assumed to interact with the entire heat structure. This is a limitation that can result in excessive wall-to-fluid heat transfer whenever a stratified fluid condition is present in the volume. Consider, for example, a core boil-off situation where a well-defined core mixture level declines below the top of the core. As the level falls through the elevation span of a core cell, the fuel rod-to-fluid heat transfer will not degrade until the cell is almost completely empty. This problem may be overcome by using more extensive axial core nodalization such that the error introduced is acceptable. A related average-fluid-condition limitation regards wall-to-liquid heat transfer in highly-voided hydrodynamic cells. In this situation, the calculated heat transfer is often insufficient to dry out the liquid, and as a result liquid droplets remain in the flow. This problem cannot be circumvented with added noding.

This section discusses general and specific practices for using heat structures. In a model, heat structures are referenced by a heat structure/geometry number (termed CCCG) and a sequence number within the CCCG. As a general practice, it is recommended that the CCCG correspond to a hydrodynamic volume to which it is connected. Note that this correspondence is not required; however, if it is used, then interpretation of the code output is greatly facilitated because heat structures and hydrodynamic cells bear the same identifying numbers.

As an example, consider a reactor vessel downcomer that is modeled using 6-cell pipe component number 570. Heat structures should represent the reactor vessel wall, thermal shield, and core barrel. Because the geometries of the vessel wall, thermal shield, and core barrel are different (i.e., their cross sections and materials are different), it will be necessary to use three separate heat structure/geometries to represent them. In this example CCCG = 5701 might be



used to represent the vessel wall, 5702 the thermal shield, and 5703 the core barrel. Within each of these heat structure/geometries the user would specify six heat structures, consistent with the six axial hydrodynamic cells. For each CCCG, heat structure 1 would connect to hydrodynamic cell 570010000, heat structure 2 would connect to hydrodynamic cell 570020000, and so on. Eighteen heat structures are therefore specified using a minimum of input, and the heat structure numbers shown in the output can be easily correlated with their locations. In this example, heat structure 5701006 is easily recognized as representing the reactor vessel wall adjacent to the sixth downcomer hydrodynamic cell.

Heat structure data are input in three sections. The first section dimensions the input and provides general data regarding the heat structures. The second section provides input data common to all heat structures in the heat structure/geometry group. The third section provides data unique to each individual heat structure. These inputs and their effects are now discussed separately.

#### 4.7.1 General Heat Structure Input and Dimensioning Data

General heat structure data are entered on heat structure card 1CCCG0000, where CCCG is the heat structure/geometry number. The data on this card dimensions the input. The parameter NH specifies the number of heat structures input for this heat structure/geometry. The number of radial mesh points and the geometry type (rectangular, cylindrical, or spherical) are also specified.

The steady-state initialization flag is an important input that is a frequent source of errors. If this flag is set to 0, the mesh point temperatures entered with the heat structure input are used for the initial condition. If this flag is set to 1, the initial mesh point temperatures are calculated by RELAP5 for a consistent steady-state solution with the boundary conditions specified (such as fluid temperatures, code-calculated heat transfer coefficients, and internal heat sources). Note that initial temperatures must be entered so that input processing may be satisfied, even if the 1 flag is used.

The left boundary coordinate must be input. The value entered here is the reference point from which the remainder of the geometry is specified. For rectangular geometries, zero may be entered, and all remaining geometrical specifications become the distance from the left surface. A recommended convention is to use the left surface as the primary and innermost heat transfer surface, although there is no requirement to do so. For example, a flat plate with a convective boundary condition to a fluid on one side and insulated on the other would be modeled with the fluid on the left surface and an insulated condition on the right surface. In this case,  $x = 0$  represents the fluid/plate surface and a value equal to the plate thickness represents the insulated boundary. For a cylindrical pipe with fluid inside, the left coordinate would be set to the inner radius of the pipe and the right surface would equal the outer radius of the pipe. The coordinate references for spherical geometries are treated in the same manner as for the cylindrical geometry. For fuel rods, it is standard practice to use a left coordinate of 0 (representing the centerline of the rod) and to specify an adiabatic condition on the left surface.

The remaining fields on card 1CCCG0000 indicate reflood options. Limited user experience data are available as a resource for the RELAP5 reflood models. Similarly, the gap conductance, metal-water reaction, and fuel cladding deformation models have limited user experience.

On restart problems, all heat structures in a CCCG heat structure geometry may be deleted from the problem by entering

```
1CCCG000 delete
```

#### 4.7.2 Heat Structure Input Common to All Structures in the Group

Card 1CCCG100 identifies the mesh location and format flags. A 0 mesh location flag indicates that the heat structure mesh, composition, and source distribution data are input as a part of this heat structure. To conserve input for cases where these data are shared among many heat structures, they only need to be input once for one heat structure/geometry group. A mesh location flag of the CCCG from that group is specified for the other inputs.

The mesh format flag is a source of user confusion. This flag concerns the manner in which the data pairs needed to lay out the heat structure mesh are to be input. Two options are available. The first option (mesh format = 1) lists pairs of the number of intervals in the region and the right boundary coordinates. The second option (mesh format = 2) lists pairs of distances and intervals. In both cases, the specifications begin at the left surface and work toward the right surface.

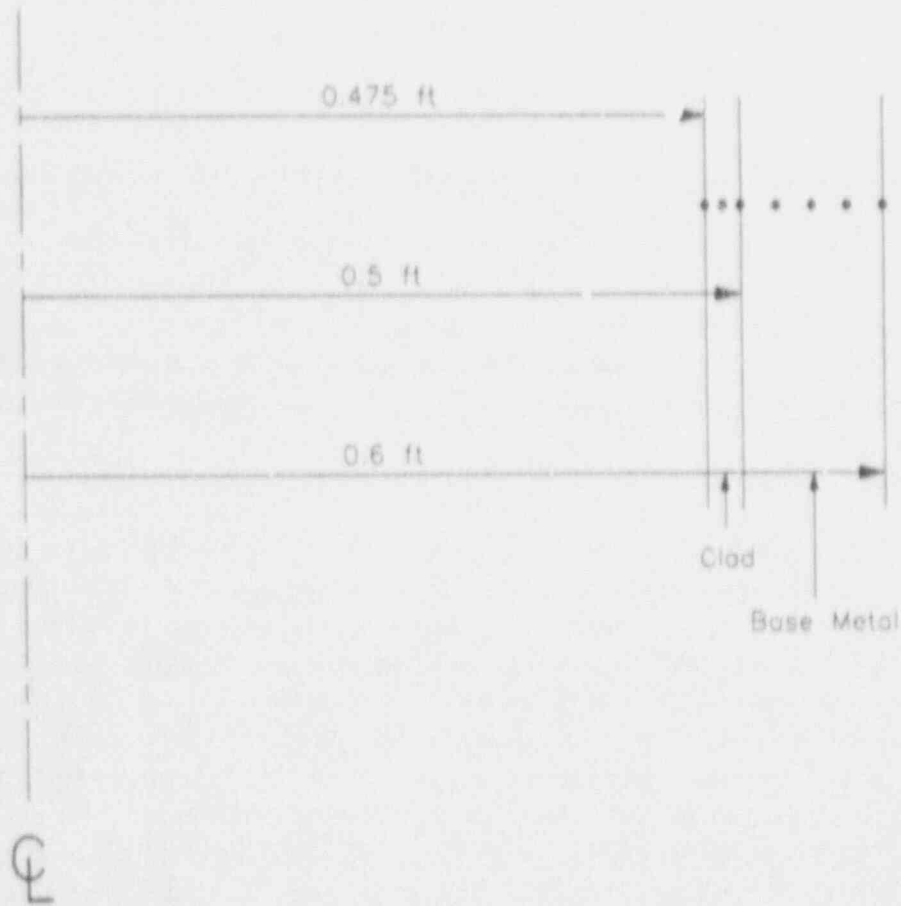
To illustrate the mesh format options, consider the following example: modeling a pipe with a cladding on the inner surface as shown in Figure 4-2. The cladding inside radius is 0.475 ft, the cladding/pipe interface is at a radius of 0.5 ft, and the pipe outer radius is 0.6 ft. A heat structure mesh is desired where one node is located on the inner surface, one node is in the center of the cladding, one node is at the clad/pipe interface, three evenly spaced nodes are within the pipe wall, and one node is on the outer surface. There will be six mesh intervals between the seven mesh points. For this problem, a left coordinate of 0.475 ft is specified. Using mesh format option 1, the remaining mesh points are specified as follows:

```
1CCCG101 2 0.5 4 0.6
```

This statement is to be read "from the left coordinate of 0.475 ft, use 2 evenly-spaced intervals through a coordinate of 0.5 ft, then use 4 evenly-spaced intervals through a coordinate of 0.6 ft." With this input, the code places the nodes at a radii of 0.475, 0.4875, 0.5, 0.525, 0.55, 0.575 and 0.6 ft. Note that the right surface is defined by the last entry, in this example at a radius of 0.6 ft. With mesh format 2, the distance between nodes and the number of such intervals would be specified for this problem as follows:

```
1CCCG101 0.0125 2 0.025 6
```

This statement is to be read "from the left coordinate of 0.475 ft, use interval thicknesses of 0.0125 ft through interval 2, then use interval thicknesses of 0.025 ft through interval 6." It is



NO40-CDF-0881-05

Figure 4-2. An example of mesh format dimensions.

recommended that the user select one of these methods and use it exclusively to avoid input errors caused by mixing the two formats. Furthermore, mesh format 2 is recommended because it is consistent with the format used for heat structure compositions and heat source distributions.

The heat structure compositions are specified using pairs of material composition identifiers and interval numbers. The composition number is the index corresponding to a set of material properties that are entered elsewhere in the input listing. Continuing the above example, consider that the cladding is stainless steel with composition number 7 and the pipe is carbon steel with composition number 8. This data would be input using

```
1CCCG201 7 2 8 6
```

This is to be read "use stainless steel through interval 2 and carbon steel through interval 6."

The distribution of heat sources among the heat structure intervals is specified using the same format. This input is needed even if no internal heat sources are modeled, in which case zeros may be entered. Pairs of relative source values and interval numbers are entered. The relative source values merely determine how the absolute internal source power for this heat structure (defined later in the heat structure specification) is to be distributed radially.

#### 4.7.3 Heat Structure Input Specific to Individual Structures

Initial temperature data are required, regardless of the initial condition flag status on card 1CCCG0000. A number of options are available and are controlled by the initial temperature flag. If the flag is 0, -1, or missing, then temperatures must be input as a part of the heat structure input data. To use temperatures input with another heat structure, an initial temperature flag equal to the CCCG of that heat structure is input. If the flag is 0, then temperatures are entered until there is one for each mesh point. It is assumed that each of the heat structures in the group uses the same initial temperatures. If the initial temperature flag is -1, then data are continued to be input until a temperature has been specified for each mesh point in each of the heat structures in the group. To allow the code to initialize the temperatures, the input data requirements may be met by using an initial temperature flag of 0 and specifying dummy temperatures. For example, for a 10 node heat structure, input

```
1CCCG401 300. 10
```

The left and right boundary condition cards specify the fluid volumes to which the heat structure is connected, and the heat transfer surface areas. In addition, these cards allow the user to implement an absolute boundary condition, such as a surface temperature or surface heat flux.

Difficulties have been encountered in the past by users who have mixed boundary condition types within a heat structure geometry group. As a result, it is recommended within each heat structure geometry group that all left boundary condition types be the same and that all right boundary condition types be the same. A set of left and right boundary conditions is needed for each of the heat structures in the heat structure/geometry group. Note that each of these heat structures shares the common cross-sectional geometry described in Section 4.7.2. A zero entry is used when representing an adiabatic or insulated boundary condition.

The "increment" entry is frequently misunderstood. The increment is used with the sequential expansion data entry format to compress data into a minimum number of cards. For example, if input is needed for five heat structures connected in sequence to volumes 120010000 through 120050000, then a boundary volume of 120010000 is entered and an interval of 10000 is specified. With this input, the boundary volume for heat structure 1 is 120010000, the boundary volume for heat structure 2 is 120020000 (120010000 + 10000), and so on.

The heat transfer surface area may be specified in one of two ways as determined by the surface area code. By using the 0 code, the surface area is entered directly as the following word. By using the 1 code, RELAP5 will automatically calculate the surface area for cylindrical and spherical geometry types based on the "factor" entered as the following word. In cylindrical geometries, the factor entered is the cylinder length. In spherical geometries, the factor is the fraction of a whole sphere (e.g., 0.5 is used to represent a hemisphere). As an example, consider the situation where the heat transfer from 10,000 cylindrical fuel rods is to be modeled. In this case, the cross section of a single fuel rod is defined using the input described in Section 4.7.2. A surface area code of 1 is used on the boundary condition card and a factor equal to 10,000 times the length of the fuel rods is entered.

The source data cards are used to specify the power generated within each heat structure. This determination is made by starting with the total power specified by the "source type." The input power may come from a reactor kinetics routine, a control variable, or a table input. The power deposited within each heat structure is defined by the product of the total power and the internal source multiplier. By using the direct heating multipliers for the left and right boundary volumes, a portion of the total power may be deposited within the fluid, such as for gamma heating. Note that the power calculated here is distributed within each heat structure as provided on the 1CCCG300 source distribution cards described in Section 4.7.2. The total of the internal source multipliers and direct heating multipliers over all heat structures in a core should equal 1.0.

The additional left and right boundary cards are used to specify the heated diameters for each heat structure and to provide data needed for the new RELAP5/MOD3 heat transfer package. Since these models are new, user experience is limited at this time. It is suggested that the recommendations in the input data requirements document regarding default input be followed (Carlson et al., 1990a).

## 4.8 General Tables

General tables are used to conveniently implement various numerical functions into a problem. A general table is entered using cards of the format 202TTTNN where TTT is the table number and NN is the sequence number of the data input. Note that data must be entered for any table that is referenced elsewhere in the problem; however, not all tables entered need to be referenced.

The first data table card entered, 202TTT00, specifies the table type, optional trip, and modification factors as described in the input data requirements manual (Carlson et al., 1990a). Available table types include power, heat transfer rate as a function of time, heat transfer coefficient as a function of temperature, temperature as a function of time, reactivity as a function of time, and normalized area as a function of normalized length.



A common user error involves misunderstandings regarding conversion factors when using tables with a type other than reactivity as a function of time. It is recommended that the user carefully check the implied units for the table type to be employed and then, as a part of the model checkout process, the user should double-check the performance of the table model.

A general table commonly is used to supply core power data as a function of time after reactor trip. An example table for this application is shown in Figure 4-3. The example problem is performed using British units; therefore, the core power is specified as 2700 megawatts in "factor 2" of Table 900. The table operates based on trip 1722 that turns true when the reactor trips. As long as trip 1722 is false, the table normalized power associated with the -1 time value is used. In this case, 1.0 is used. Following reactor trip, the normalized power declines with time, representing the effects of scram rod insertion and decaying heat. Note that the time argument in the table is to be read "time in seconds after the occurrence of trip 1722 turning true." Therefore, it is recommended that the reactor trip be modeled using a "latched" trip (see Section 4.4).

## 4.9 Reactor Kinetics

This section provides guidance to the reader regarding the use of the RELAP5 space-independent "point" reactor kinetics model. The point kinetics formulation uses core-average fluid conditions, weighting factors, and feedback coefficients to determine a total reactivity for driving the kinetics calculation of total core power. Once the total core power has been determined, it is then distributed among the fuel heat structures in an invariant manner. For many simulation problems, a point kinetics formulation may be an adequate approximation of the physical processes. The user should, however, carefully consider the adequacy issue for the particular application. If it is determined that point kinetics is inadequate, then it may be possible, through an iterative process between RELAP5 and a more functional kinetics code, to converge upon the true solution.

Core power may be specified in the model by using an input table, a control variable, or by the reactor kinetics model. This selection is made according to the "source type" entered as the first word on the heat structure source data cards (format 1CCCG0701). If a source type less than 1000 is entered, then a heat source based on a general table with the same number is used. If a source type greater than 10000 is entered, then the heat source is based on the control variable equal to the source type minus 10000. The reactor kinetics model is used to power a heat structure when source types 1000, 1001, or 1002 are specified. See the input data requirements manual for the option most appropriate for your application (Carlson et al., 1990a).

An example reactor kinetics input data set, shown in Figure 4-4, will be used to illustrate use of this code feature. The input values shown are not to be considered representative of actual data for any plant. Users should employ data appropriate for their particular applications.

The reactor kinetics input begins with card 30000000, which specifies POINT (the only option available at this time) followed by the feedback type. Three feedback options are available: SEPARABL, TABLE3, and TABLE4. The feedback data required to be input are determined by the selection. The SEPARABL option is the simplest and most frequently used.

```

-----
*                               table no. 900 = power
*-----*
*table      table type  trip no.   factor 1   factor 2
20290000   power       1722      1.0        2700.
*
*table
20290001   -1                1.0
20290002   0                 1.0
20290003   0.1              0.8382
20290004   0.5              0.2246
20290005   0.8              0.1503
20290006   2.0              0.09884
20290007   4.0              0.08690
20290008   8.0              0.07375
20290009   10.0             0.06967
20290010   30.0              0.05060
20290011   60.0              0.03977
20290012   80.0              0.03604
20290013   150.              0.02987
20290014   300.              0.02565
20290015   800.              0.02073
20290016   1500.             0.01749
20290017   2500.             0.01489
20290018   3000.             0.01401
*

```

Figure 4-3. An example of core power data - function of time.

```

*****
* reactor kinetics example input *
*****
30000000 point separabl
30000001 gamma-ac 1848.24e6 0.0 329.412 1.0 1.0
*
* scram table
30000011 920
*
* moderator density reactivity table
30000501 6.3725 0.006
30000502 40.0000 0.100
30000503 48.8710 0.120
30000504 48.0000 0.130
30000505 70.3065 0.250
*
* fuel temperature doppler reactivity table
30000601 32.0 0.2
30000602 4500. 0.1
*
* volume weighting factors and temperature coefficients
* vol cell wt fun react $
30000701 514010000 0 .07391 -0.0089
30000702 514020000 0 .18250 -0.0089
30000703 514030000 0 .24359 -0.0089
30000704 514040000 0 .24359 -0.0089
30000705 514050000 0 .18250 -0.0089
30000706 514060000 0 .07391 -0.0089
*
* fuel temperature doppler coefficients
* ht struct wt fun react $
30000801 5141001 0 .1670 -5.592e-4
30000802 5141002 0 .1670 -5.592e-4
30000803 5141003 0 .1670 -5.592e-4
30000804 5141004 0 .1670 -5.592e-4
30000805 5141005 0 .1670 -5.592e-4
30000806 5141006 0 .1670 -5.592e-4
*
* reactivity scram table
20292000 reac-t 554
20292001 0.0 0.0
20292002 1.0 0.0
20292003 2.0 -0.35
20292004 4.0 -6.55
20292005 5.0 -9.60
20292006 1.e6 -9.60
*

```

Figure 4-4. An example of a reactor kinetics input data set.

With SEPARABL, the data entered specify the moderator density, moderator temperature, and fuel temperature feedback information (the volumes and heat structures from which the densities and temperatures are used, and the reactivity feedback coefficients for each). With this option, a change in one of the three parameters does not affect the others.

The TABLE3 and TABLE4 options require the input of multi-dimensional tables that allow the user to specify interactions among the reactivity feedback functions (e.g., the dependence of the moderator density feedback as a function of the moderator temperature may be modeled). With TABLE3, a three-dimensional table linking moderator density, moderator temperature, and fuel temperature feedback is entered. With TABLE4, a four-dimensional table linking the above three effects with boron concentration is entered. The SEPARABL option is most often selected, simply because the data needed to input TABLE3 and TABLE4 feedback are unavailable.

In addition to the required input for the selected feedback option type, the user may specify additional reactivity components by indicating what tables or control variables are to be used for that purpose. In the Figure 4-4 example, Table 920 (input at the bottom of the input list) specifies the reactivity of the scram rod in dollars as a function of time after reactor trip (trip 554). The table is implemented as a reactivity component on card 30000011.

Card 30000001 specifies the constants that control the kinetics calculation. Note that the initial reactor power is entered in watts regardless of whether British or SI units are used in the problem. This convention differs from other code features where power is entered in megawatts for British units.

The total reactivity feedback in dollars is calculated by the code using the formulation

$$\begin{aligned} \text{total reactivity} = & \text{initial reactivity} - \text{bias reactivity} + \text{reactivity from tables} \\ & + \text{reactivity from control variables} + \sum [\text{WF R}(\rho) + a_w T_w] \\ & + \sum [\text{WF R}(T_f) + a_f T_f]. \end{aligned}$$

In this equation, WF is the weighting factor entered on card series 30000701 for the hydrodynamic volumes and on card series 30000801 for the heat structures. The "a" coefficients are entered on these same cards. The R functions are those specified on card series 30000501 (density) and 30000601 (fuel temperature). The subscript "w" indicates "for the water" and the subscript "f" indicates "for the fuel." The first sum is over the user-specified hydrodynamic cells and the second sum is over the user-specified heat structures.

In the Figure 4-4 example, the core is made up of six hydrodynamic cells (51401 through 51406) and six fuel rod heat structures (5141001 through 5141006). The moderator density reactivity is weighted by the center-peaked cosine axial core power profile, and the fuel temperature weighting is linear. For the fuel temperature feedback calculation, the average temperature of the fuel pellet is used. This average temperature is distinguished from the average heat structure temperature (which includes fuel, gap, and cladding regions) by the heat structure composition data input on card series 1CCCG201 (CCCG is the heat structure/geometry identifier). The user is referred to the users input manual for this card series (Carlson et al.,

1990a). Structure regions with positive composition numbers are included in the average temperature calculation while regions with negative composition numbers are not.

It is important for the user to carefully consider the total reactivity equation. The moderator temperature, moderator density, and fuel temperature reactivities are calculated using the initial fluid and heat structure conditions. To this, the initial values of any table-entered and control-variable-entered reactivities are added. Next, the "initial reactivity" is added (this was input by the user). This sum is exactly and automatically balanced by the code with the bias reactivity such that the initial total reactivity is zero. In other words, the code assumes that the reactivity must be zero at time zero, and biases the calculation to force that condition. This code-calculated bias reactivity is displayed at the end of the input processing edit and is carried as a constant reactivity contribution throughout the calculation.

The authors' preference for entering reactivity feedback is to select the SEPARABL option, defeat its reactivity effect by entering zero for the reactivity coefficients in the required feedback input, and then calculate total reactivity using control variables. One advantage of this method is that the components of reactivity are more easily understood by the user because they are independently calculated and tracked. The component reactivities are summed into a total reactivity, and a single control variable is then used to drive the reactor kinetics calculation. Another advantage of this method is that each of the reactivity components may be biased to zero at the initial condition such that the component reactivity changes during a calculation are easily displayed and interpreted. In this way, the reactivity components, the user-input initial reactivity, and the code-calculated bias reactivity all are zero at the initial time.

In practice, before attempting to incorporate reactor kinetics into a model, it is recommended that a satisfactory steady state first be obtained with the desired core power specified through an input table rather than by kinetics. This step ensures that the initial core conditions are appropriate so that little change in reactivity will occur when the calculation is started. When this has been accomplished, the power source is shifted from the input table to the kinetics package (by changing the source types on the core heat structure cards). A calculation is then performed to attain an adequate full-power steady-state condition with the kinetics package activated. At this point, the user may find that small deficiencies in the original steady-state conditions may cause the kinetics-calculated steady core power to be marginally different than the desired value. This situation may be remedied by implementing a shim control reactivity (via a control variable) to drive the model to the exact core power desired. This shim control system would then be defeated (by specifying a constant control variable with a value equal to the final value of the shim reactivity) before beginning any transient simulations.

## 4.10 Control Variables

RELAP5 control variables are an extremely flexible and useful feature of the code. Contrary to the name, control variables are suited to many functions in a calculation beyond the simulation of a control system. Control variables may be used to relate diverse types of calculated data, perform mathematical and logical operations, and cause actions to occur in the model.



The user must first understand the control variable input and its functions. Consider the following control variable input developed for the purpose of calculating the difference in mass flow rates between junctions 15601 and 15602 in lbm/s and limiting this difference to between 0 and 5000 lbm/s:

```
20515600 delmdot sum 2.2046 1000.0 3 0. 5000.  
20515601 0. 1. mflowj 156010000  
20515602 -1. mflowj 136020000
```

Control variables are entered using cards of the format 205NNNXX, where NNN is the control variable number and XX is the input card sequence number. Many different types of control variables are available. The format for the 00 sequence card is identical for all of the types, while the format of the 01, 02, ... sequence cards is different for each type. Two format conventions, original and extended, are available for entering control variable data [see the user input data requirements manual (Carlson et al., 1990a)]. All control variables in a problem must use the same convention. Examples of control variable applications shown here use the original format.

In the above example, control variable 156 has been assigned the name "delmdot," a descriptive abbreviation for differential mass flow. The sum control variable type has been indicated with a scale factor of 2.2046, the conversion factor from kg/s to lbm/s. An initial value of 1000. has been specified and the "0" entry following it means to use the specified initial value (an entry of 1 would indicate that the code should calculate the initial value based on the initial values of the mass flow rates). The "3" entry means that minimum and maximum values are to be applied. The remaining fields indicate the minimum allowable value is 0 and the maximum allowable value is 5000. References to the external data and coefficients to be used appear on sequence cards 01 and 02. The 0 entry is an additive constant while the 1 and -1 entries are the coefficients.

As a transient proceeds, the mass flow rate through junction 15602 will be multiplied by -1 and added to the product of the junction 15601 mass flow rate and the coefficient 1. A frequent source of user error is the oversight that all internal references to data within control variables are performed in SI units. Thus the references to the junction mass flow rates return values in kg/s, not lbm/s, even if the problem is being solved in British units. The scale factor 2.2046 converts the differential mass flow in kg/s to lbm/s.

Note that the minimum and maximum apply to the final value of the control variable, after the scale factor has been applied. Moreover, the user should remember that the output of a control variable by definition is considered dimensionless by the code. In this example, the user has created control variable 156 to represent the differential mass flow rate in lbm/s; however, to the code, the output of the control variable has no dimension. Therefore, the user must ensure that units are properly accounted for.

The user should be aware that control variables are evaluated in numerical order according to the control variable number. If a reference is made to control variable "A" within control variable "B," then the value of "A" will be as of the previous timestep if  $A > B$  and as of the current timestep if  $A < B$ . In some situations, understanding this convention is critical. Finally, the user should understand that control variables are solved last, after the hydrodynamic and heat

transfer solutions have been obtained. Therefore, the values of the control variables on any timestep reflect the thermal-hydraulic conditions for the current timestep. Conversely, actions taken as a result of control variables attaining a particular status will not occur until the following timestep.

A summary of the control variable types and brief statements regarding their functions appears in Table 4-3. Generally, additive constants and multiplicative coefficients may be implemented within each control variable, in addition to the functions specified. Using appropriate combinations of control variables, virtually any algebraic, logical, or functional action may be taken in the model. The user is referred to the input data requirements manual for the exact formulas for each control variable type (Carlson et al., 1990a).

When a user first sets up a model, it is recommended that control variables be developed to provide continuous indications of various important process variables. Examples of these variables for a PWR include steam generator secondary-side mass, primary-to-secondary heat transfer, and steam generator and pressurizer levels. When used in this way, the control variable provides a convenience to the user because these frequently-devised parameters are calculated by the code as a part of the calculation. The advantage is that the user does not need to assemble these data using a post-processing routine, an often cumbersome and time-consuming job.

Beyond convenience, situations arise where data must be calculated using a control variable or they will be lost. These situations regard any process involving integration (e.g., tracking an integrated break flow). It is not possible to reconstruct an accurate record of integrated break flow using a post-processing routine because the RELAP5 restart/plot file contains the mass flow data only at the user-requested plot point time interval. All data for time steps between these points are therefore lost. To track integrated break flow, an INTEGRAL control variable is used to integrate the break mass flow parameter. With this method, the break junction mass flow rate is integrated by the code at each time step and thus, the output of this control variable represents a true indication of integrated break flow.

To illustrate the process of using control variables in an actual problem, consider the following rather complex simulation problem. Core power is calculated using the reactor kinetics model, and one of the reactivity components needed is based on the control rod position. The control rod reactivity worth is known as a function of its position. The initial position is known, and it will be assumed its reactivity is zero at the initial position. The control rod has two modes of operation: prior to, and after scram. Prior to scram, the rod performs a power shim function at a limited maximum rate of travel, attempting to control the reactor at the desired operating power. After scram, the rod takes on a safety function, and is driven into the core via a spring mechanism. This mechanism provides an initial 6-g acceleration to the rod, decays linearly to 1-g when the rod has been driven in 60 mm, and then has a constant 1-g acceleration thereafter. For this problem, a normalized rod position of 0 represents fully withdrawn, and a position of 1 represents fully inserted.

The control system input developed to simulate the control rod reactivity is shown in Figure 4-5. This input leads to determining the current normalized control rod position (the "new" position, CNTRLVAR 957) and the reactivity associated with that rod position. The

**Table 4-3.** Control variable types and their functions.

Control Variable Type	Function
SUM	Add parameters
MULT	Multiply two parameters
DIV	Divide one parameter by another
DIFFRENI	Differentiate a parameter response; Exact initial value must be specified
DIFFREND	Differentiate a parameter response; No initial value needed, an approximation
INTEGRAL	Integrate a parameter
FUNCTION	Access a user-input table with an independent variable and return the dependent variable
STDFNCTN	Standard functions (e.g., trigonometry) of an independent variable
DELAY	Use the previous time value of a parameter
TRIPUNIT	Binary operator keyed to a trip status
TRIPDLAY	Binary operator (equals 0 if trip is false and equals time trip last turned true if trip is true)
POWERI	Raise a function to an integral power
POWERR	Raise a function to a real power
POWERX	Raise one function to a power defined by another function
PROP-INT	Proportional-integral Laplace operator
LAG	Lag Laplace operator
LEAD-LAG	Lead-lag Laplace operator
CONSTANT	Specifies a constant value
PUMPCTL, STEAMCTL, FEEDCTL	Specifies pump speed, steam, and feed control for self-initialization
SHAFT	Links turbines, pumps, and loads

```

$-----$
*ctlvar      name      type      factor      init      f c      min      max
20594300 "timest"      sum      1.          .0025 0 0
*
*ctlvar      a0      coeff      variable name      parameter no.
20594301      0.          1.          time                0
20594302      -1.         -1.         cntrlvar            944
$-----$
*ctlvar      name      type      factor      init      f c      min      max
20594400 "oldtime"     sum      1.          30.    0 0
*
*ctlvar      a0      coeff      variable name      parameter no.
20594401      0.          1.          time                0
$-----$
*ctlvar      name      type      factor      init      f c      min      max
20594500 "noscrum"    tripunit  1.          1.     1 0
*
*ctlvar      trip no.
20594501      -510
$-----$
*ctlvar      name      type      factor      init      f c      min      max
20594600 "scram"      tripunit  1.          0.     1 0
*
*ctlvar      trip no.
20594601      510
$-----$
*ctlvar      name      type      factor      init      f c      min      max
20594900 "powerr"     sum      1.          0211123 0 0
*
*ctlvar      a0      coeff      variable name      parameter no.
20594901      -350       1.e-6     rktpow             0
$-----$
*ctlvar      name      type      factor      init      f c      min      max
20595000 "lagerr"     lag      1.          02135538 0 0
*
*ctlvar      tau-1      variable name      parameter no.
20595001      0.5       cntrlvar            949
$-----$
*ctlvar      name      type      factor      init      f c      min      max
20595400 "shimsp"    sum      1. 1.69348e-6 0 3 -.001586 .001586
*
*ctlvar      a0      coeff      variable name      parameter no.
20595401      0.          7.93e-5  cntrlvar            950
$-----$
$      table 956 - scram rod speed as function of time after trip
$-----$
*table      table type      trip no.      factor 1      factor 2
20295600      reac-t      510          1.          1.
*
*table      time      reactivity
20295601      -1.          0.
20295602      0.           0.
20295603      0.005       0.2931
20295604      0.01        0.5802
20295605      0.015       0.8555
20295606      0.02        1.1133
20295607      0.025       1.3485
20295608      0.03        1.5561
20295609      0.035       1.7321
20295610      0.04        1.8727
20295611      0.045       1.9752
20295612      0.0491     2.0292
20295613      0.06        2.1360
20295614      1.0         11.3480

```

Figure 4-5. An example of control system input to simulate control rod reactivity.

```

$-----$
*ctlvar      name      type      factor      init      f c      min
20595600 "scramsp"      function 0.651466      0.      0 1      0.
*
*ctlvar      srch arg name      srch arg. no.      table no.
20595601      time      0      956
$-----$
*ctlvar      name      type      factor      init      f c      min      max
20595900 "shimsp"      mult      1.      1.69348-6      0
*
*ctlvar      variable name      parameter no.      variable name      parameter no.
20595901      cntrlvar      954      cntrlvar      945
$-----$
*ctlvar      name      type      factor      init      f c      min      max
20596000 "scramsp"      mult      1.      0.      0
*
*ctlvar      variable name      parameter no.      variable name      parameter no.
20596001      cntrlvar      956      cntrlvar      946
$-----$
*ctlvar      name      type      factor      init      f c      min      max
20596100 "rodspeed"      sum      1.      1.69348-6      0
*
*ctlvar      a0      coeff      variable name      parameter no.
20596101      0.      1.      cntrlvar      959
20596102      1.      cntrlvar      960
$-----$
*ctlvar      name      type      factor      init      f c      min      max
20596500 "deltapos"      mult      1.      4.2337-9      0
*
*ctlvar      variable name      parameter no.      variable name      parameter no.
20596501      cntrlvar      961      cntrlvar      943
$-----$
*ctlvar      name      type      factor      init      f c      min      max
20596700 "newpos"      sum      1.      .278668      0 3      0.      1.
*
*ctlvar      a0      coeff      variable name      parameter no.
20596701      0.      1.      cntrlvar      968
20596702      1.      cntrlvar      965
$-----$
*ctlvar      name      type      factor      init      f c      min      max
20596800 "oldpos"      sum      1.      .278668      0 3      0.      1.
*
*ctlvar      a0      coeff      variable name      parameter no.
20596801      0.      1.      cntrlvar      967
$-----$
$ table 970 - control rod reactivity as function of normalized rod
$ position [biased to zero at initial position]
$-----$
*table      table type      trip no.      factor 1      factor 2
20297000      reac-1
*
*table      time      reactivity
20297001      0.      3.93
20297002      0.1218      3.50
20297003      0.2195      2.33
20297004      0.2790      0.
20297005      0.4391      -6.27
20297006      0.6098      -18.18
20297007      0.7805      -28.89
20297008      1.      -32.78
$-----$
*ctlvar      name      type      factor      init      f c      min      max
20597000 "rodreac"      function      1.      .01290627      1 3      -32.78      3.93
*
*ctlvar      srch arg. name      srch arg. no.      table no.
20597001      cntrlvar      967      970
$-----$

```

Figure 4-5. (continued).



reactivity output (CNTRLVAR 970) is an evaluation of the rod position vs. the worth table (Table 970) at the new rod position. The current value of CNTRLVAR 970 therefore is used as a component dollar reactivity (see the reactor kinetics description in Section 4.9).

The control variable logic is required to determine the current or new normalized rod position at each time step. The new position is calculated by adding the change in normalized rod position during the current timestep (of length  $\Delta t$ ) to the old rod position according to the formula

$$\text{new rod position} = \text{old rod position} + [(\text{shim speed}) \text{ or } (\text{scram speed})]\Delta t$$

Referring to Figure 4-5, the current time step size is first calculated in CNTRLVAR 943. This is accomplished by subtracting the problem time on the previous time step (CNTRLVAR 944) from the current problem time (time 0). This technique takes advantage of the order in which control variables are evaluated. When evaluating CNTRLVAR 943, which references CNTRLVAR 944, the latter has a value as of the previous time step.

Binary operators are developed (in CNTRLVAR 945 and 946) to represent the scram status (defined elsewhere in the problem using trip 510). CNTRLVAR 945 has a value of 1 before scram and a value of 0 afterwards; the reverse is true for CNTRLVAR 946. These binary operators are used to determine which of the rod speeds (shim or scram) is to be used.

The shim speed is determined by the power error, which is the difference between the current core power and the desired core power. The power error is calculated with CNTRLVAR 949, which takes the difference between the current reactor power (rktpow 0) and the desired core power (350 MW). For stability, this error is lagged by 0.5 s in CNTRLVAR 950. The lagged power error is then related to the current shim rod speed in CNTRLVAR 954. A maximum normalized rod travel rate of  $0.001586 \text{ s}^{-1}$  was simulated in the shim mode. This condition was met by specifying these minimum and maximum values in CNTRLVAR 954. The coefficient  $7.93\text{e-}5$  was selected to provide a maximum rod travel rate when the magnitude of the core power error exceeds 20 MW.

Next, the rod speed in the scram mode is calculated using CNTRLVAR 956. This is accomplished by hand calculating the rod speed as a function of time after scram (based on the initial 6-g acceleration and linear acceleration decline to the gravity-drop situation). The output of this hand calculation is recorded in Table 956, which lists the normalized rod speed as a function of the time since the scram trip 510 turned true. Note that a "reac-t" table type is specified. This was done only to non-dimensionalize the table. The dependent variable is actually normalized rod speed, not reactivity. CNTRLVAR 956 simply evaluates Table 956 and returns a normalized scram rod speed.

The inverse binary operators developed in CNTRLVAR 945 and 946 are now applied to the shim and scram speeds, respectively in CNTRLVAR 959 and 960. At all times, one of these speeds will be zero. The two speeds are added together in CNTRLVAR 961 that now represents the current normalized rod speed.

The change in normalized rod position for the current time step is calculated in CNTRLVAR 965, which multiplies the current normalized rod speed (CNTRVAR 961) by the time step size (CNTRLVAR 943). The new normalized rod position is calculated by adding the change in rod position to the rod position in the previous time step. This new position (CNTRLVAR 967) is then used to determine an associated rod worth by evaluating Table 970 with CNTRLVAR 967. CNTRLVAR 970 is used as a dollar reactivity in the kinetics calculation.

This example is intended to demonstrate the power and flexibility that RELAP5 control variables afford the user for modeling complex operations.

#### **4.11 RELAP5 Internal Plotting Routine**

RELAP5 contains a rudimentary routine for generating the data needed for plotting calculational results. The capabilities of the internal plotting package are not considered adequate for most applications. An external post-processing plotting routine is used at the INEL for this purpose.

## 5. PRESSURIZED WATER REACTOR EXAMPLE APPLICATIONS

This section provides example RELAP5 modeling applications for PWRs. The purpose of this section is to provide guidance for developing general plant models that may be used for analyzing a wide variety of small break LOCAs and operational transients. The user is cautioned that no model is generally applicable for simulating all transient scenarios. Care should be taken so that modeling and nodalization are appropriate for the particular application.

### 5.1 Westinghouse Plants (Base Case)

This section provides guidance for modeling Westinghouse PWRs. The specific example discusses a three-loop plant design; modeling of two- and four-loop designs is similar. A complete input listing for the example plant is included in Appendix B. The following subsections discuss the example model by regions.

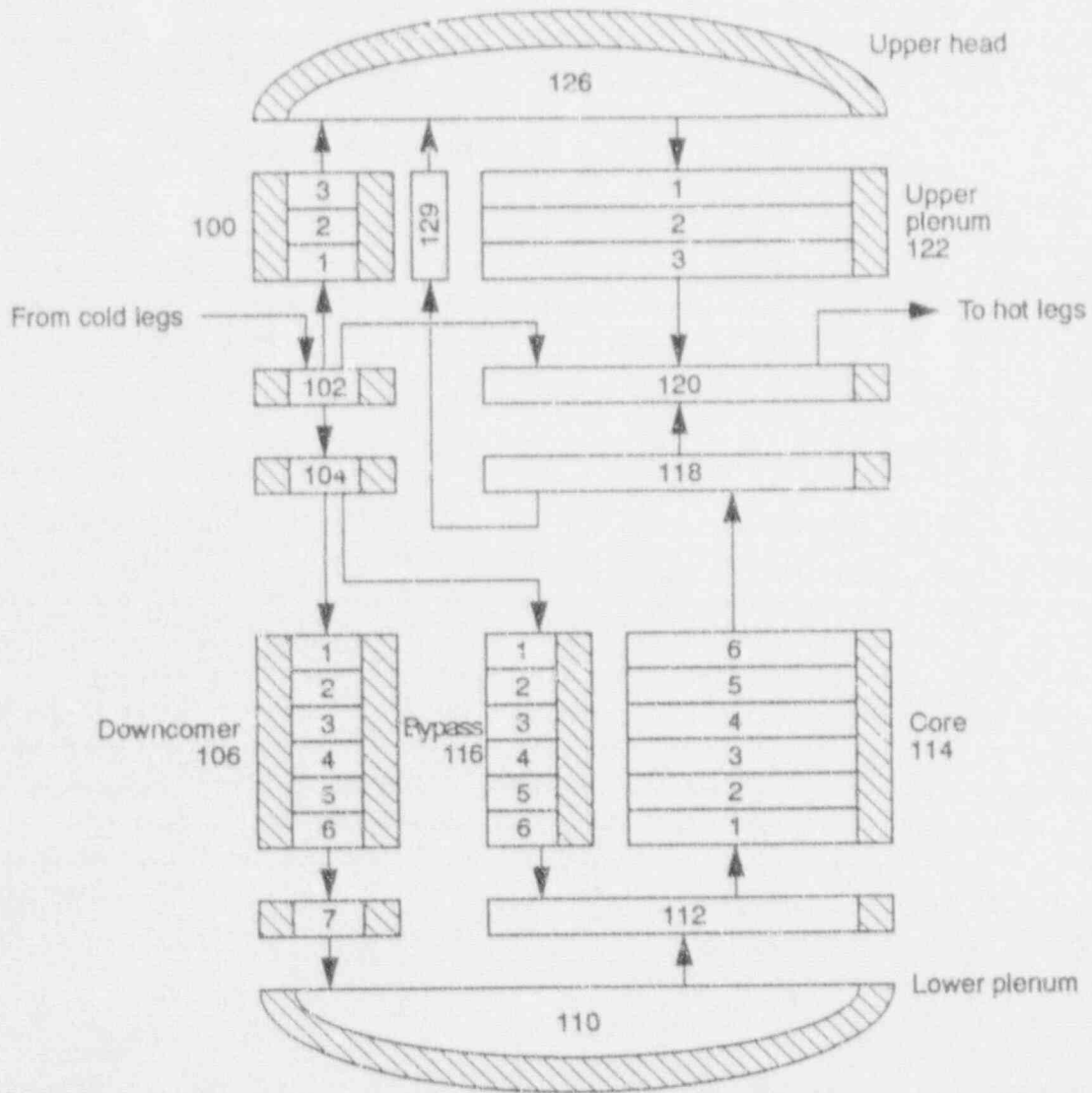
#### 5.1.1 Reactor Vessel

Reactor vessel nodalization is shown in Figure 5-1. Flow enters from the cold legs into the reactor vessel downcomer annulus in branch 102. The modeler should note that the hydrodynamics associated with branch and pipe components are identical. The branch component may have its own associated external junctions, while the pipe component may have only internal junctions (therefore relying on single junctions, valves, or branch junctions for external connections). The modeler's choice between pipe and branch components is one of convenience. The primary reactor vessel flow path is downward through branch 104 and annulus 106 to the lower plenum, component 110. An annulus component is identical to a pipe component except an annular flow regime map is used. A portion of the inlet flow is diverted around the downcomer through bypass pipe 116. This bypass is a large volume, but low flow region between the core former plates and core barrel. In the example plant the bypass is a region of downward flow, effectively a downcomer bypass. In some plants this region is in upward flow and is a core bypass.

Another portion of the inlet flow is diverted upward through pipe 100 and through the upper reactor vessel bypass nozzles into the upper head, branch 126. Still another portion of the inlet flow is bypassed directly to the hot leg through the slip-fit between the core barrel assembly and reactor vessel wall at the hot leg nozzles. This path is represented by the junction from branch 102 to upper plenum branch 120.

Core inlet branch 112 recombines the downcomer and bypass flows before entering the heated core that is represented by pipe 114. The upper plenum is represented by branches 118 and 120, and by pipe 122. Branch 129 represents the guide tubes that route a portion of the core exit flow from the upper plenum to the upper head.

Note that in the example PWR model, the hot and cold legs are connected to the reactor vessel at the inlet and outlet faces of reactor vessel components. This model was assembled prior



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Figure 5-1. Nodalization of reactor vessel.

to the availability of the crossflow junction. Standard practice now calls for the hot and cold leg connections to be made with crossflow junctions (see discussion in Section 3.4.5). To upgrade the vessel noding in Figure 5-1 for this recommendation, it would be necessary to change the elevation spans of branches 102 and 120 such that their midpoints are at the elevation of the hot and cold leg centerlines.

The desired flow splits through the various reactor vessel bypasses generally are attained in the model by adjusting the calculated flow losses (forward and reverse loss coefficients) as needed to best represent the actual losses associated with orifices and complex geometries. To minimize iterations, this process should proceed from the flow paths with the largest flows to those with the smallest flows. In general, when representing small leakage paths between large volumes (e.g., the nozzles between pipe 100 and branch 126), the modeler should not use a highly reduced junction flow area (e.g., that of the orifice itself). Instead, a junction flow area equal to that of the smaller of the two adjacent volumes should be used along with an increased loss coefficient as needed to limit the flow to the desired value.

Heat structures are used to represent the fuel pins, the major internal structures (thermal shield, core barrel wall, core former plates, guide tube walls, etc.), and the reactor vessel cylindrical shell and spherical heads. These heat structures allow simulation of inter-region heat transfer, such as between the core and bypass regions through the core former plates.

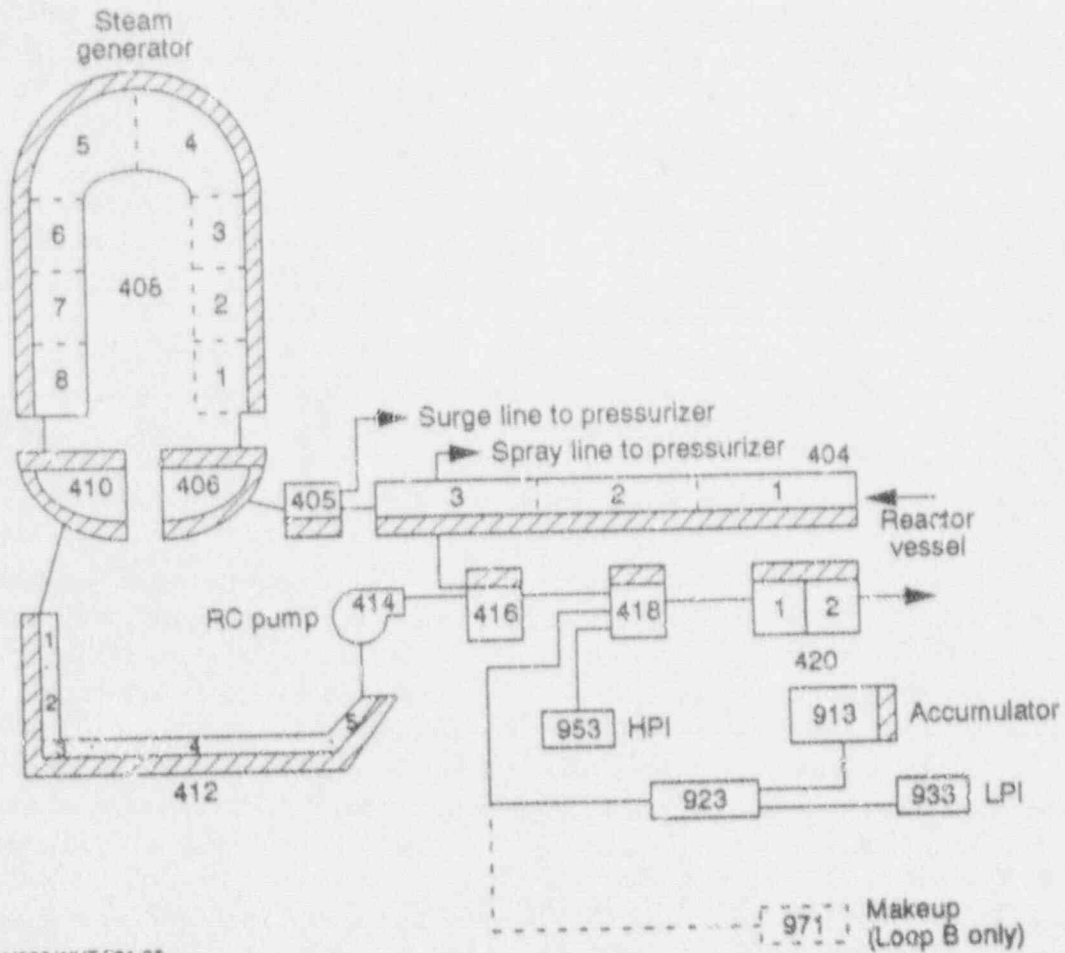
The noding for the reactor vessel shown in Figure 5-1 represents the standard nodalization scheme used at the INEL for small break LOCA simulations. The elevations of the junctions between nodes are consistent between parallel flow paths (such as the downcomer, bypass, and core regions); this scheme was developed to prevent numerical oscillations between parallel channels during early development of the code. Nodalizing the core with six axial cells is a compromise scheme allowing observation of core uncovering, yet being relatively economical. If an accurate simulation of the core uncovering process is needed, then the user is advised to use a finer nodalization near the top of the core. Additionally, six-cell core noding provides some resolution of core axial void profiles that affect reactor-kinetics core power calculation. If very accurate void feedback simulation is needed, then the user should consider finer nodalization, core-wide. Nodalization of the upper plenum and upper head regions provides sufficient resolution of flashing phenomena and liquid levels in these regions during accident simulations.

### 5.1.2 Hot and Cold Legs and Steam Generator Primaries

Standard INEL nodalization for one of the primary coolant loops is shown in Figure 5-2. Flow from the reactor vessel enters hot leg pipe 404 and progresses through branch 405 into the steam generator inlet plenum, branch 406. It was necessary to break the hot leg into two components so that the pressurizer surge line may be attached at the proper location. It is not possible to connect an external junction (such as the surge line) at a pipe internal junction (such as would have occurred if the entire hot leg had been modeled with a single 4-cell pipe).

Pipe 408 represents the many thousands of steam generator tubes. These tubes are lumped into a single component using the same philosophy as is explained in Section 5.5 for the lumping of two coolant loops. Representing the steam generator tube primaries with an 8-cell pipe





4355-WHT-181-03

Figure 5-2. Nodalization of primary coolant loops (Loop C shown).

component is a nodalization scheme that compromises between calculational fidelity and expense. This scheme has proven to be generally useful, however the modeler should individually consider the nodalization requirements for the problem to be modeled. The tube nodalization scheme shown may not be sufficiently detailed to model phenomena associated with reflux cooling and greatly reduced secondary-side levels. Branch 410 represents the steam generator outlet plenum. Modeling of the steam generator secondary region is described in the following section.

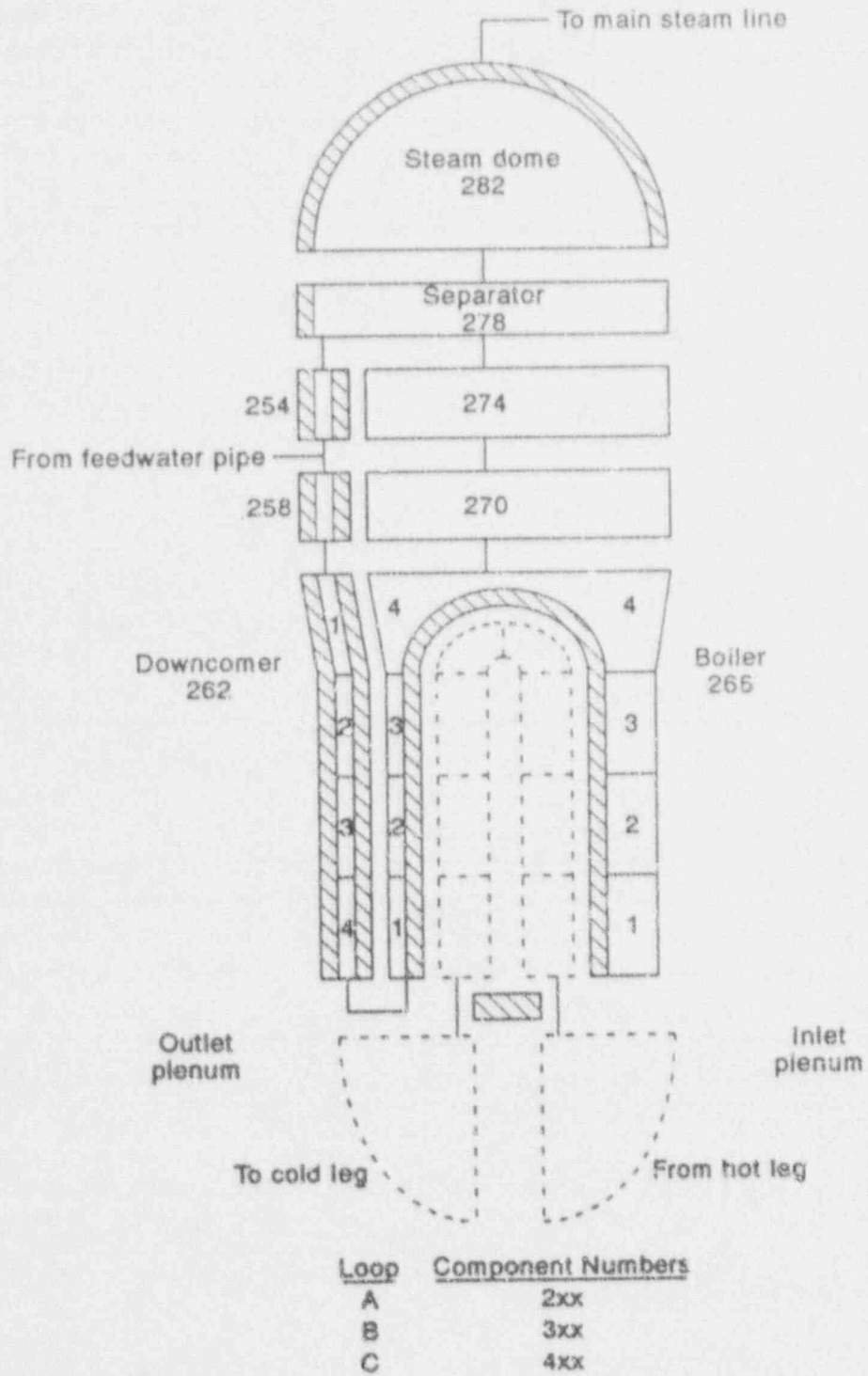
Pipe 412 represents the pump suction cold leg. To ensure proper simulation of behavior in the loop seal region, cell 4 of this pipe is input as horizontal. This orientation allows the formation of horizontally stratified flows at the bottom of the loop seal. It is recommended that at least one horizontal cell be used for simulating loop seal phenomena. Cells 1, 2, 3, and 5 of pipe 412 provide sufficient vertically-oriented calculational cells for simulating the formation of liquid levels in the loop seal region and for simulating countercurrent flow limiting phenomena. The pump component is described separately in Section 5.1.5.

The pump discharge cold leg is modeled with branches 416 and 418 and pipe 420. This nodalization scheme has proven suitable for simulating horizontal stratification of fluid within the cold legs during loss-of-coolant accidents. The nodalization also provides for proper simulation of the fluid temperature distribution in the region; the junction between the branches is located such that the ECC injection site is correctly modeled. The user should remember that RELAP5 provides a one-dimensional representation of the flow and therefore is not capable of resolving thermal stratification of warm and cold liquids within the same pipe. Therefore, although the model may observe the bulk movement of cold ECC liquid toward the core, it is not capable of observing a stream of cold liquid residing in the bottom of the horizontal pipe. The high and low pressure ECC functions are modeled with pairs of time-dependent volumes and junctions. The ECC fluid injection temperature is specified by the time-dependent volume while the injection flow rate is specified as a function of the cold leg pressure by the time-dependent junction. This method allows simulating the head/flow characteristics of the centrifugal ECC pumps. An example of the method is provided in Section 4.6.4. A RELAP5 accumulator component is used to simulate the injection behavior of the nitrogen-charged accumulators. This lumped-parameter component model mechanistically represents the tank and surge pipe hydrodynamics, heat transfer from tank wall and water surface, water surface vaporization to the gas dome, and gas dome condensation. The accumulator model is described in Section 4.6.10.

Heat structures are employed to model the hot and cold leg piping walls, the steam generator plena heads, the plena separation plate, the tubesheet, and the steam generator tubes.

### 5.1.3 Steam Generator Secondaries

Standard INEL nodalization for one of the steam generator secondaries is shown in Figure 5-3. Modeling of the steam generator primary region was described in the previous section. In the secondary region, main feedwater enters the steam generator downcomer annulus at branch 258 where it is combined with the recirculation liquid flow returning from the separator (component 278) through downcomer annulus branch 254. The combined flow descends through the downcomer (annulus 262) and enters the boiler (pipe 266). Note that the axial nodalization was made consistent between the tube primary, boiler, and downcomer regions. The use of four



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Figure 5-3. Nodalization of steam generators.

axial hydrodynamic cells in the boiler region has proven generally useful. However, finer nodalization of the boiler region may be needed for simulating phenomena associated with reflux cooling mode and significantly depleted steam generator secondary inventory. The user is advised to carefully consider the nodalization needs for a particular application. Overall steam generator performance is dependent on correctly simulating the recirculation ratio (the boiler flow rate divided by the feedwater/steam flow rate) because it controls the heat transfer process on the outside of the tubes. The flow losses associated with the horizontal baffles in the tube bundle region often are not well-characterized. Therefore, if a satisfactory initial agreement with the desired recirculation ratio is not attained, adjustment of input form losses in the boiler may be justified.

The two-phase mixture exiting the boiler region flows through the mid-steam generator regions (branches 270 and 274) before entering the separator (branch 278). The separator model is idealized and includes three modes of operation that are determined by the separator void fraction. The void fractions defining these modes are input by the user. At low void fractions, the separator model reverts to a normal branch component, allowing carryover of liquid into the steam dome (branch 282). At high void fractions, the separator also reverts to a normal branch component, allowing carryunder of steam through the liquid return path into the downcomer. At intermediate void fractions, an idealized separation process is calculated: all liquid is returned to the downcomer and all vapor is passed to the steam dome. A detailed discussion of separator modeling appears separately in Section 4.6.6.1.

The modeler should carefully consider the elevation chosen to locate the separator. In the steam generator model, separation will take place based on the void fraction in the separator volume, whose lower and upper elevations are user-specified. In the actual plant, separation is accomplished in two stages (swirl-vane separators and steam dryers) that reside at two different elevations. Therefore, the model is at best a compromise of the actual separation processes. The selections of separator elevation span and void limits determine when recirculation is interrupted as the secondary mixture levels decline. Note that these levels decline significantly when a steam generator's heat load is reduced, such as following a reactor trip. The levels also decline significantly during transients where the secondary inventory is depleted, such as during a secondary-side LOCA.

Heat structures are employed in the model to represent the steam generator tubes, the cylindrical shell and spherical head, the cylindrical baffle separating the boiler and downcomer regions, and the internals of the separator and steam dome regions.

It often is difficult to obtain a satisfactory agreement with steam generator full-power conditions. The difficulty arises because the heat transfer coefficient calculated on the outside surface of the steam generator tubes is based on general vertical-pipe correlations rather than correlations that account for the swirling flows present within the tube bundle region. The swirling flow pattern results because horizontal baffles in the boiler direct the flow back and forth across the tube bundle instead of allowing the flow to proceed axially (vertically upward) through the boiler. The effect of this discrepancy is that tube heat transfer is understated by the code, resulting in excessively high calculated primary coolant temperatures (the temperatures increase until the core heat is driven across the tubes). Since the source of the calculated error is understood (i.e., a general heat transfer correlation is not appropriate for this application) it is

recommended that the modeler "adjust" the heat transfer on the outside of the tubes to remedy the discrepancy.

The recommended adjustment is to reduce the input heated equivalent diameter on the heat structure cards for the outer tube surface. It is recommended that instead of using the boiler region hydraulic diameter as the heated diameter that the minimum tube-to-tube spacing (the distance from the outside of a tube to the outside of its neighbor) be used. If the modeler decides not to follow this recommendation, it will be necessary to compromise an important parameter (such as using a lower secondary pressure, higher primary temperature, or lower feedwater temperature) to simulate full-power steam generator operation.

#### 5.1.4 Pressurizer

Standard INEL nodalization for the pressurizer and its associated systems is shown in Figure 5-4. The pressurizer upper head is modeled with branch 340 and the pressurizer cylindrical body and lower head are modeled with 7-cell pipe 341. Generally, good agreement with experimental and plant data has been attained for slow and fast pressurizer insurges and outsurges with this nodalization. The surge line is modeled with 3-cell pipe 343.

The functions of the two power-operated relief valves (PORVs) are lumped into valve 344 and those of the three code safety valves are lumped into valve 346. The valves open in response to a significant primary coolant system overpressure. Operation of these valves, including their hysteresis effects, is simulated using the methods described in example 2 in Section 5.4.2. The pressurizer spray system is modeled with single volumes 335, 337, and 339, and valves 336 and 338. The spray valves open in response to a mild primary coolant system overpressurization. Operation of these valves is simulated using logic similar to the PORV and code safety valves. The flow area of all valves is that necessary for delivering the rated flow capacity at the rated upstream pressure.

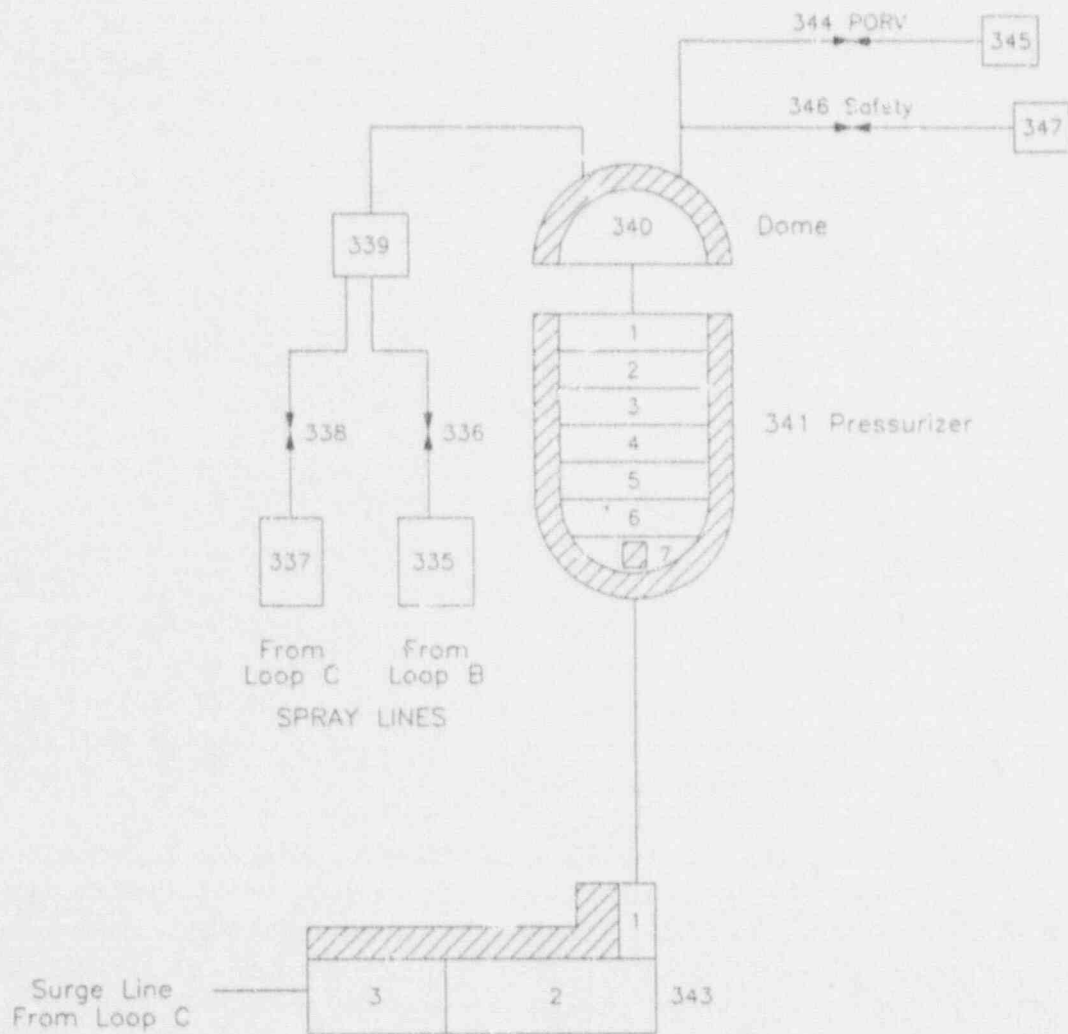
Heat structures are used to represent the cylindrical pressurizer shell and its spherical lower and upper heads, and the pressurizer surge line pipe wall. Heat structures are also used to simulate operation of the pressurizer heaters. Heater power is increased in response to an underpressurization of the primary coolant system pressure and is terminated if a low pressurizer level is sensed.

#### 5.1.5 Reactor Coolant Pump

A reactor coolant pump forces the coolant flow in each of the three coolant loops. The pump component 4.4 is located as shown on the loop nodalization diagram, Figure 5-2. A complete discussion of pump modeling is given in Section 4.6.8 and will not be repeated here.

In the example PWR model, the pump speed is controlled as follows. First, to obtain a satisfactory steady-state condition, the pump speed may be varied as needed (via a control variable) to attain the desired loop flow rate. Next, once the proper steady condition has been calculated, the pump speed is held constant until a reactor coolant pump trip is implemented (such as by operator action). When the pump is tripped, its speed coasts down as determined by the pump inertia, the hydrodynamic loads, and the pump-bearing friction.





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Figure 5-4. Nodalization of pressurizer.

### 5.1.6 Balance-of-Plant Systems

The model includes feedwater and steam balance-of-plant systems. Sections 5.1.6.1 and 5.1.6.2, respectively, describe modeling of these systems. Figure 5-5 shows a nodalization diagram of the feedwater and steam systems.

In the example model, the feedwater system extends from the condenser hotwell to the steam generator feedwater inlet nozzles. The decision to include or exclude the feedwater system from a model of a Westinghouse plant should be made based on the transient calculations that are planned. Since feedwater is normally tripped immediately following a reactor trip, many transients may be simulated adequately simply by specifying the feedwater temperature and flow at the steam generator using a time-dependent junction/time-dependent volume pair. However, for transients involving extended feedwater injection following reactor trip (e.g., steam generator overfeed events), a more complete feedwater system modeling may be needed. In addition to retaining model generality, upgraded feedwater system modeling provides more representative simulations of feedwater temperature and flow rate at the steam generator inlets than could be provided with a simple model.

In the example model, the steam system extends from the steam generator outlet nozzles to the turbine stop and steam dump valves. Theoretically, the steam and feedwater systems may be joined into a closed loop by simulating the turbine stages and extraction paths (the turbine component is described in Section 4.6.6.3). In practice, however, the steam system model usually is truncated as shown in Figure 5-5 to avoid the modeling complexities of closing the loop. This simplification is warranted because the initiation of most transients includes rapid closure of the turbine stop, turbine control, or main steam isolation valves. Therefore, complete modeling of the steam system is typically an expensive model luxury.

**5.1.6.1 Feedwater System.** The standard INEL feedwater system nodalization is shown in Figure 5-5. This nodalization has proven satisfactory for simulating the pressure and thermal gradients within the feedwater system during normal operation and during accident conditions. Sufficient model detail is included to properly simulate the distribution of fluid temperatures and pressures within the system. Generally, feedwater system conditions are expected to be single-phase liquid. However, correctly simulating the fluid temperature and pressure distributions can be important for predicting fluid flashing behavior during accidents involving depressurization of the steam generator secondary system.

Time-dependent volume 822 represents the condenser hotwell; fluid conditions here include low temperature water at a vacuum pressure. The condensate pumps draw fluid from the hotwell (component 824 lumps the two condensate pumps together). Section 4.6.8 provides a complete discussion of pump modeling. The pump discharges through a set of five low pressure heaters, modeled with components 830 and 840; a bypass line around the low pressure heaters is also modeled. Pipe components with heat structures representing the heater tubes model the heaters. Heat sources (simulating the heating from turbine extraction steam) are modeled within the tube materials. Note that the heat source is interrupted during transient events as a result of steam flow interruption; this effect is included in the model. Since stored energy in the piping may be an important consideration for feedwater temperature during transients, the model includes heat structures representing the feedwater system piping walls.

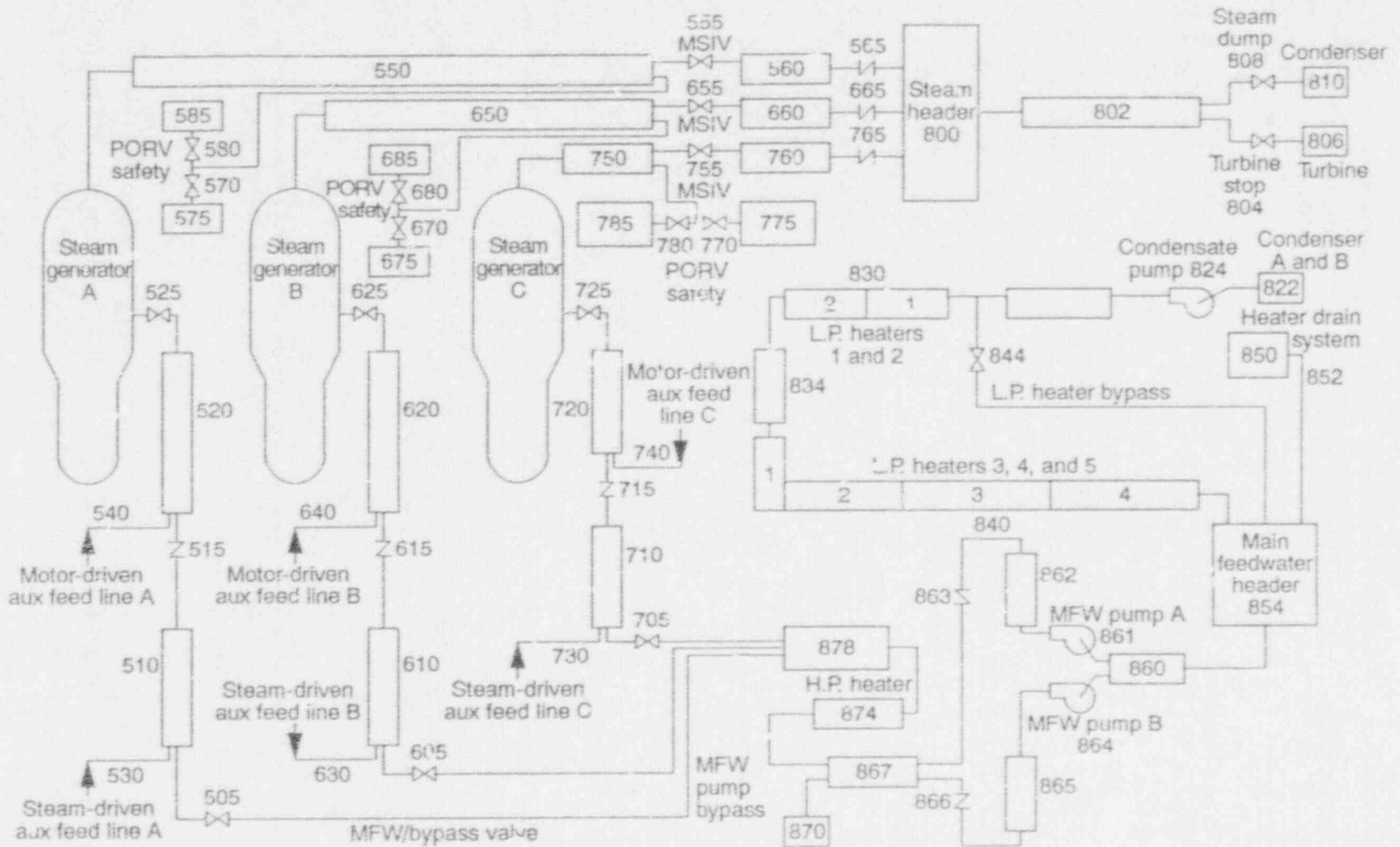


Figure 5-5. Nodalization of feedwater and steam systems.

Downstream from the low pressure heaters, the main feedwater flow is combined in component 854 with flow through the bypass (if open), and with the heater drain flow (if available). The heater drain flow results from steam condensation within the heaters. When the steam flow is interrupted during transient events, the heater drain flow ceases.

Both main feedwater pumps were represented in the model since it was desired to simulate transients when only one of the pumps was tripped. To model the check valves at the outlets of the main feedwater pumps, it was necessary to include single volumes 862 and 865 in the model. The pump model includes its own inlet and outlet junctions so it is not possible to include a check valve directly within the pump component. A main feedwater pump recirculation line is included in the model for use during periods when the main feedwater valves are completely closed.

Discharges from the two main feedwater pumps are combined before flowing through the high pressure heater (component 874). Modeling for the high pressure heater is comparable to that described above for the low-pressure heaters. Valves 505, 605, and 705 represent the main feedwater valves (Section 5.1.7.2 describes control of these valves). Components 510, 520, 610, 620, 710, and 720 model the main feedwater lines to the individual steam generators. Flow from the steam- and motor-driven auxiliary feedwater systems is modeled with time-dependent junction components.

**5.1.6.2 Steam System.** The standard INEL steam line nodalization is shown in Figure 5-5. The nodalization includes very long cells representing the steam lines between the steam generators and the turbine. This noding has proven adequate for simulating all transients for which these regions remain steam-filled. This noding has also proven adequate for simulating main steam line break accidents, in which liquid is flashed to steam within the steam generator secondary system and the vapor production sweeps liquid out the break. For this simulation, the uncertainty regarding separator performance far exceeds that involved in two phase mixture flow in long pipe volumes. The user should consider finer noding if simulation of liquid ingress is needed (such as during an extreme steam generator overflow transient).

Single volumes 550, 560, 650, 660, 750, and 760 (see Figure 5-5) represent the steam lines leading from the individual steam generators to the steam header, branch 800. The junctions between the steam generator domes and the steam lines use reduced flow areas and added flow losses to represent the steam flow restrictors at that location.

Valves 555, 655, and 755 represent the main steam line isolation valves. These are modeled using motor valve components that allow specification of a closure rate. Valves 565, 665, and 765 represent the steam line check valves that prevent flow from one steam generator from exiting a break in another steam generator.

Time-dependent volume 806 sets the boundary conditions representing the inlet of the turbine, and servo valve 804 represents a combination of the turbine stop and turbine governor valves. Prior to reactor trip, this valve modulates to control the turbine inlet pressure. Following reactor trip, the valve closes, simulating a turbine trip. The steam generator pressure boundary condition is set by the combination of (a) the time-dependent volume pressure and (b) the total flow pressure loss from the steam generator to the time-dependent volume at the normal steam flow rate. Section 5.1.3 discusses difficulties in obtaining the proper steam generator heat



removal rate at the proper steam pressure. Assuming those difficulties are circumvented, as discussed, the desired steam generator pressure is attained by adjusting the loss coefficient at the turbine stop/governor valve to compensate for incomplete turbine modeling.

Servo valve 808 models the steam dump (or turbine bypass) valve (Section 5.1.7.1 discusses control of this valve). Servo valves 570, 670, and 770 model the banks of safety relief valves. For each steam generator, the multiple safety valves are simulated with a single valve component that opens in steps, depending on the steam pressure and its history. The total valve flow area is sized by summing the individual valve areas needed to match the rated capacity at the rated pressure for each valve in the bank. A control variable calculation is then performed to determine the status (open or closed) of each valve. Example 2 in Section 4.4.2 provides guidance for the logic required. The binary valve statuses are multiplied by the respective normalized flow areas of the individual valves. These are summed into a control variable that represents the total valve normalized flow area (0 is fully closed and 1 is fully opened) that specifies the valve model flow area. This technique eliminates the need to model a valve and time-dependent volume component for each valve in the bank, and retains the true valve bank response characteristics. Modeling for the PORVs (components 580, 680, and 780) is comparable to that for the safety valves.

### 5.1.7 Plant Control Systems

This section discusses modeling of the more significant plant control systems. The steam dump, steam generator level, pressurizer pressure, and pressurizer level control systems are described.

**5.1.7.1 Steam Dump Control.** The purposes of the steam dump control system are (a) to permit the plant to accept sudden losses of load without tripping the reactor, (b) to remove core stored energy and residual heat following a reactor trip and bring the plant to equilibrium no-load conditions without actuation of the steam generator safety valves, and (c) to control the steam generator pressure at no-load conditions, allowing a transition to manual control. Three corresponding modes of steam dump control serve these purposes. The first two modes (load rejection and plant trip) control the valves based on the primary coolant system average temperature, whereas the third mode (steam pressure) controls the valves based on the steam generator pressure.

The load rejection controller modulates the steam dump valves (if the load rejection is greater than 70%, the steam line PORVs are also modulated) to control the primary system temperature. First, the turbine inlet pressure is linearly converted into a average primary system temperature setpoint. The filtered derivative of the pressure is used to determine its magnitude and whether or not a load rejection has occurred. If a load rejection has occurred, the controller then compares the average primary system temperature with the setpoint value and modulates the steam dump valves. Figure 5-6 shows a block diagram of this portion of the controller. Modulation of the steam dump valves is blocked if the condenser does not have sufficient vacuum, or if the primary average temperature decreases below the minimum temperature setpoint. Figure 5-7 shows valve position as a function of the temperature error. The input required to model the load rejection controller appears in control variables 800 through 815 (control variable input appears at the end of the input listing in Appendix B).



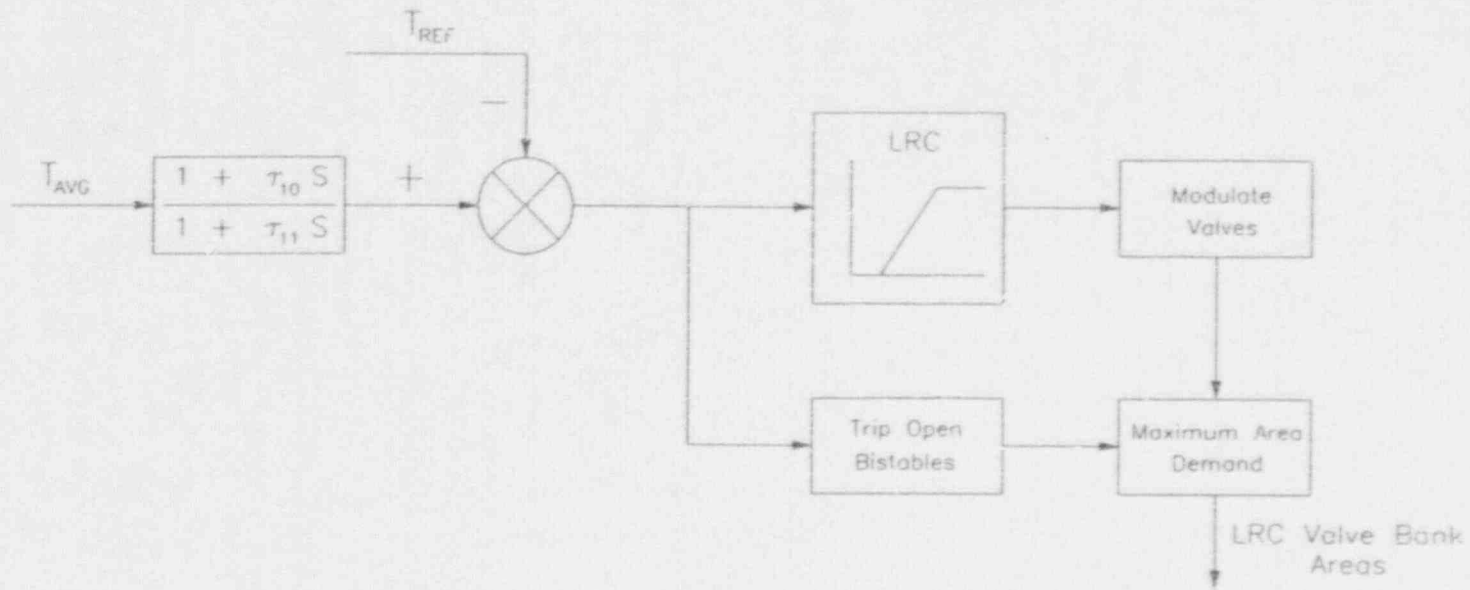
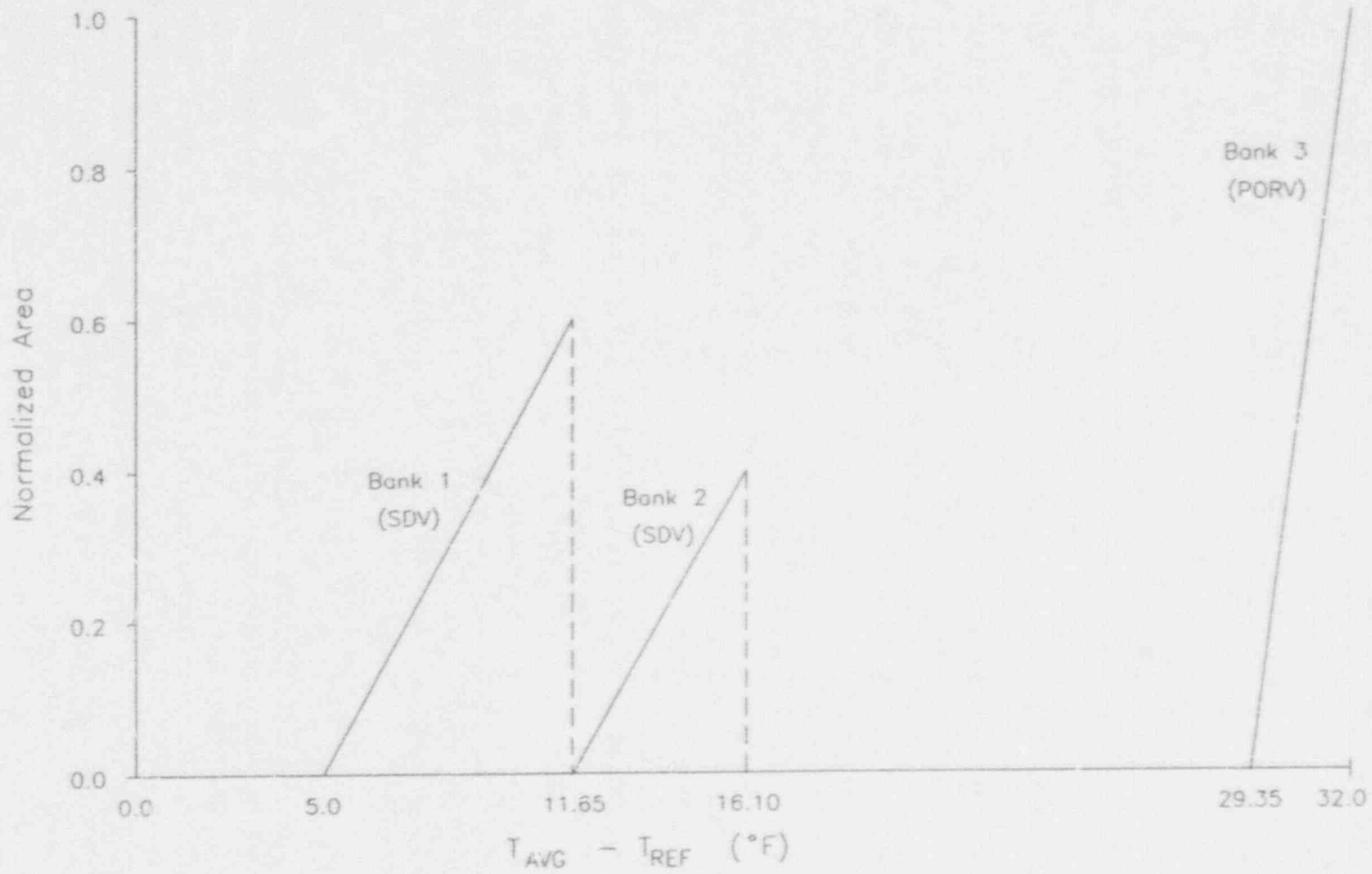


Figure 5-6. Block diagram of load rejection controller.

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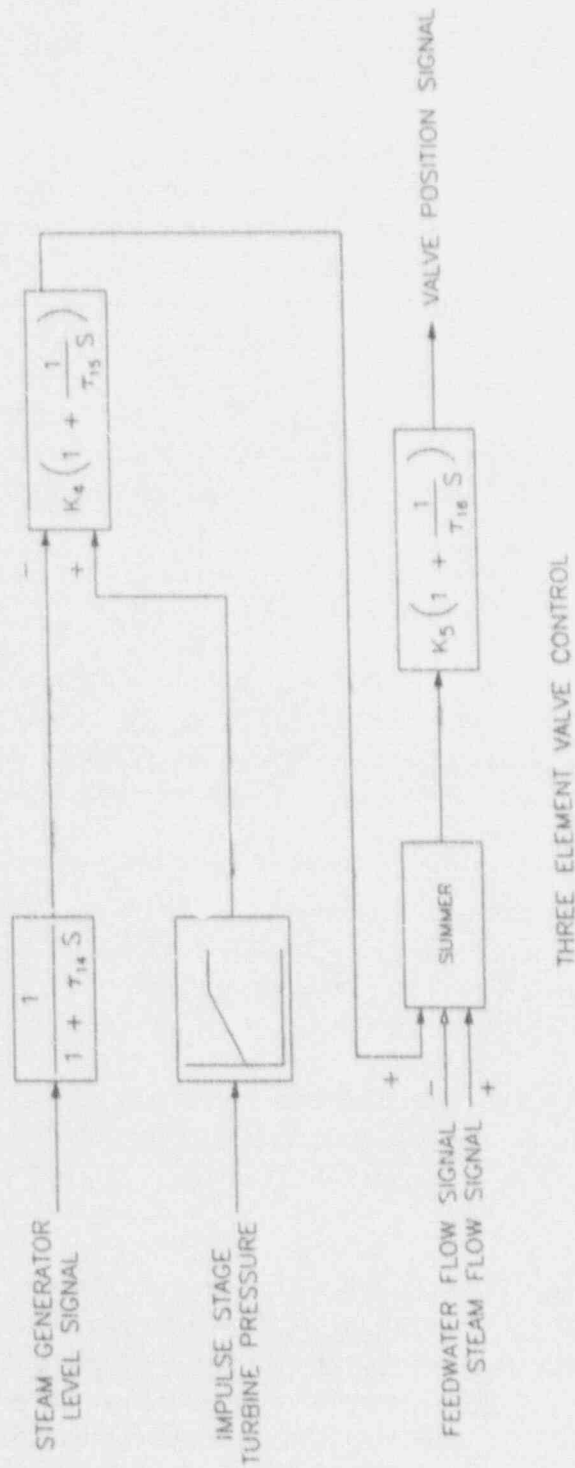
Figure 5-7. Load rejection controller valve response.

The plant trip controller modulates the steam dump valves to control the primary system temperature at the equilibrium, no-load setpoint immediately following a turbine trip. Modulation of the steam dump valves is blocked if the condenser does not have sufficient vacuum or if the average primary temperature is below its setpoint value. With the exception that the steam line PORVs are not modulated, the logic for this controller is similar to that for the load rejection controller. The input required to model the plant trip controller appears in control variables 820 through 823.

The steam pressure controller regulates the steam dump valves during hot standby operation and after the plant has been brought to its no-load setpoint temperature following a turbine trip. A proportional-integral signal that operates on the error between the current and setpoint steam pressures controls the dump valve flow area. The input required to model the steam pressure controller appears in control variables 825 through 831.

**5.1.7.2 Steam Generator Level Control.** The steam generator level control system regulates the steam generator downcomer liquid level by controlling the main feedwater valve based on three elements: current steam generator level, feedwater flow, and steam flow. Figure 5-8 shows a block diagram of the steam generator level control system. The controller first compares the current steam generator level against a current setpoint level that is a function of the current plant load (the load is inferred from the turbine impulse stage pressure). The resulting error signal is summed with the mismatch between the current feedwater and steam flow rates and that output is used to control the position of the main feedwater valve. Each steam generator employs a separate control system; the following discussion uses the level control system for steam generator A as an example.

The first step calculates the steam generator level signal. In the plant, this is accomplished by sensing the pressure difference between two taps in the steam generator secondary, and converting to a level using a reference density. In the model, the level is calculated similarly by control variables 500 through 508. The pressures at the tap locations are determined by interpolating between the two pressures at the cell centers that envelope the actual elevation of the pressure tap. The calculated level is then smoothed in a manner similar to the plant instrumentation system. Control variable 510 calculates the setpoint level, and control variable 511 calculates the level error. The error signal is then processed by a proportional-integral operator (control variable 512) and the output is summed with the feedwater/steam mass flow rate mismatch in control variable 513. The proportional-integral operator in control variable 514 calculates the feedwater valve demand signal. At this point, a series of main feedwater valve permissive tests are applied (failure of any test causes the main feedwater valve to close, regardless of the normal level control functions). These tests include (a) reactor trip and low average coolant temperature, (b) high steam generator level, (c) safety injection actuation signal, and (d) main feedwater pump trip. After the tests have been applied, control variable 523 calculates the change in the valve flow area. Control variable 524 calculates the new feedwater valve area by summing the old area (i.e. that on the last time step) with the calculated area change. For simplicity, the valve area is normalized (0 is fully closed and 1 is fully open); this allows control variable 524 to be used directly by the RELAP5 servo valve component that simulates the main feedwater valve.



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Figure 5-8. Functional block diagram of the steam generator level control system.

**5.1.7.3 Pressurizer Pressure Control.** The pressurizer pressure control system maintains the desired primary system pressure by regulating the pressurizer spray valves, relief valves, proportional heaters, and back-up heaters. The pressure error is determined by comparing the current pressurizer pressure with the setpoint pressure. The error signal is input to a proportional-integral operator whose output controls the functions of the heaters and the spray and relief valves. Figure 5-9 shows a block diagram of the pressurizer pressure control system logic. The input required to model this controller appears in control variables 210 through 226.

**5.1.7.4 Pressurizer Level Control.** The pressurizer level control system maintains the desired liquid inventory in the pressurizer. The pressurizer setpoint level is specified as a function of the primary coolant system average temperature. The level error is determined by subtracting the setpoint level from the measured level (as determined by the difference in pressure between two taps and a reference density). The pressures at the tap locations are determined by interpolating between the two calculated pressures at the cell centers that envelope the actual elevation of the pressure taps. The calculated level is then smoothed in a manner similar to the plant instrumentation system. The level error signal is input to a proportional-integral operator whose output specifies the change in the charging pump speed (and thereby the fluid addition rate to the primary coolant system). The input required to model this controller appears in control variables 200 through 206.

### 5.1.8 Modeling a Large Break Loss-of-Coolant Accident

Although LBLOCAs have been modeled at the INEL in the past using earlier versions of RELAP5 (Adams et al., 1986; Demmie et al., 1982), LBLOCA analyses haven't been performed at the INEL because RELAP5/MOD2 was declared an SBLOCA/operational transient analysis code. LBLOCA analyses have been performed by users at other locations, however.

The following summary has been compiled entirely from RELAP5/MOD2 analyses because no RELAP5/MOD3 analyses are available yet. Since major differences exist between the MOD2 and MOD3 heat transfer packages and interphase drag models, the following information is of limited usefulness. As more up-to-date information becomes available, these guidelines will be updated.

To the authors' knowledge, no studies exist that relate assessment analyses performed on scaled facilities to commercial plants for RELAP5. Consequently, the following are guidelines specific to scaled facilities such as LOFT or Semiscale and should be regarded as a starting point for a commercial plant analysis.

Some of the most extensive LBLOCA work has been done at the Institute of Nuclear Energy Research in Taiwan (Kao et al., 1988; Liang et al., 1988), the Korea Atomic Energy Research Institute (Bang et al., 1991), and the Paul Scherrer Institute (PSI) in Switzerland (Lubbesmeyer, 1991a, 1991b). Work by Lubbesmeyer is of particular interest because major simplifications to the fundamental LOFT model used by most of the other researchers were studied. Lubbesmeyer's work is based on the LOFT LP-LB-1 and LP-02-6 experimental data.



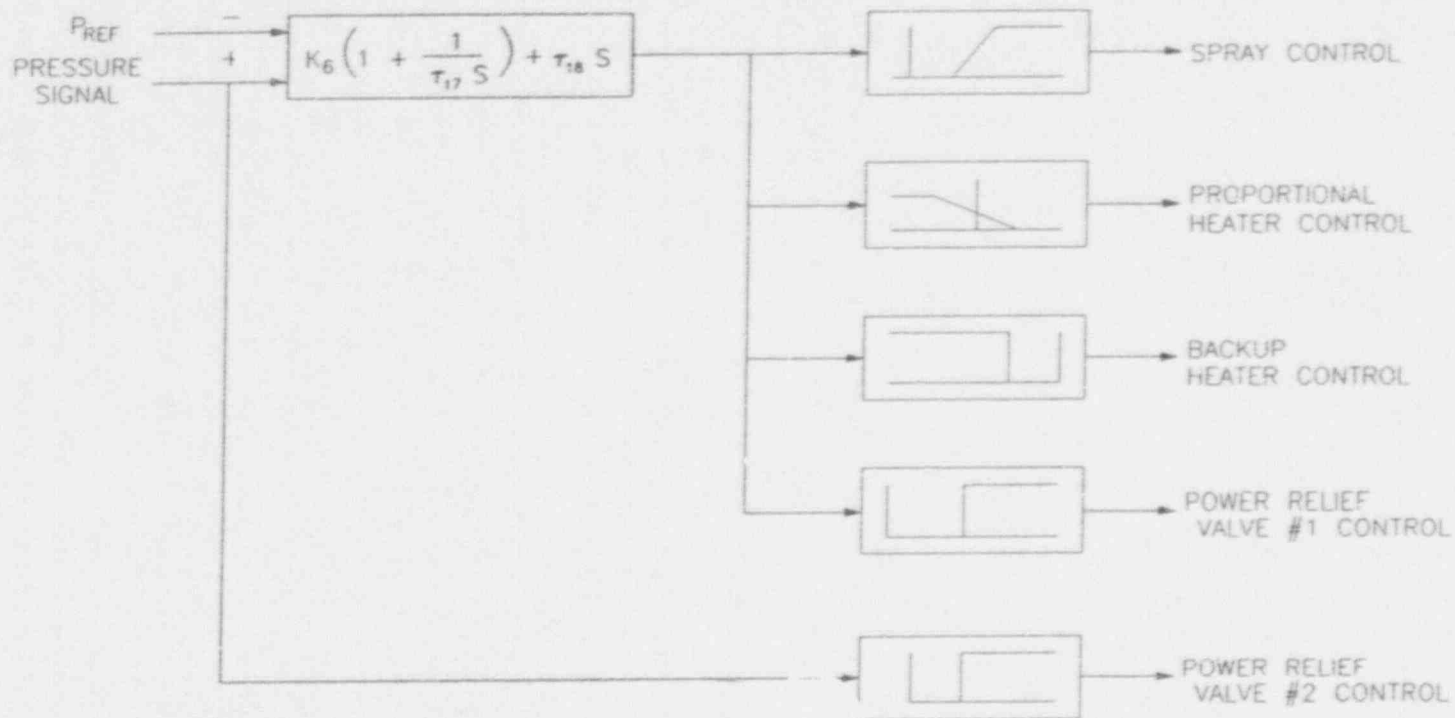


Figure 5-9. Block diagram of pressurizer pressure control system.

Lubbesmeyer's studies focused on the code's capability to simulate LBLOCA related thermal-hydraulic phenomena for various nodalizations. Lubbesmeyer began with a rather detailed nodalization (Figure 5-10) and then performed the same analysis using simpler nodalizations (Figure 5-11). The core nodalization was unchanged throughout the studies (Figure 5-12) and the vessel nodalization was only slightly modified.

The initial, detailed nodalization is shown in Figure 5-10. This model contains 18 components in the reactor vessel, including 2 components each to model the intact and broken sides of the downcomer and 3 components to model the core region. Note that the LOFT vessel downcomer was modeled by dividing the downcomer into two non-interacting equally-sized annuluses that connect with the broken and intact loops even though the LOFT facility simulates the presence of three plant loops with its intact loop. The core fuel region was modeled with the average power core zone, containing 5 cells and sized to include 79% of the total mass flow, whereas the high power zone was sized to include 16% of the total flow and contained 13 cells. Lubbesmeyer did not use any crossflow junctions in the core because preliminary calculations using the crossflow junctions had shown the quantity of mass exchange in the traverse direction to be negligible.

The remainder of the more detailed nodalization contained 20 components in the intact loop with a total of 24 cells (not including the ECCS), 3 components in the primary side of the steam generator (SG) (the tubes were modeled using 8 cells in component 515), 15 components in the secondary side of the SG, 4 components in the pressurizer and surge line (including 6 cells in component 415 to model the main pressurizer tank and 3 cells in the surge line), and 15 components to model the broken loop including 21 cells in the broken loop piping.

To explore the effect on the code's capability to calculate the important thermal-hydraulic phenomena present in an LBLOCA, Lubbesmeyer simplified the model nodalization in two steps. First, the detailed model was simplified by decreasing the number of components in the loops, the SG, and the pressurizer. The vessel and core nodalizations were not changed. The intact loop was modeled with 7 components with a total of 21 cells, the SG primary side was modeled with only 1 component (6 cells), the SG secondary side was modeled with 3 components, the pressurizer and surge line were modeled with 2 components (5 cells), and the broken loops were modeled with only 6 components, with a total of 15 cells in the broken loop pipes.

Lubbesmeyer's most simplified nodalization is shown in Figure 5-11 and differs from the previous simplification by having the same number of components in the intact loop, SG, and broken loop, but fewer cells. The number of cells in the intact loop was decreased to 10, the SG primary side was represented with only 2 cells, the SG secondary side was represented with 3 cells, and the broken loop piping was modeled with only 5 cells.

Lubbesmeyer's conclusions (Lubbesmeyer, 1991a, 1991b) concerning LBLOCA-specific nodalizations are summarized below. (Note: Portions of the conclusions that compare the calculations to the LOFT data have been removed in the editing process.):

- With respect to the computation time, the degree of specification of the nodalization (i.e., the numbers of volumes and junctions) is an important parameter. But a lower

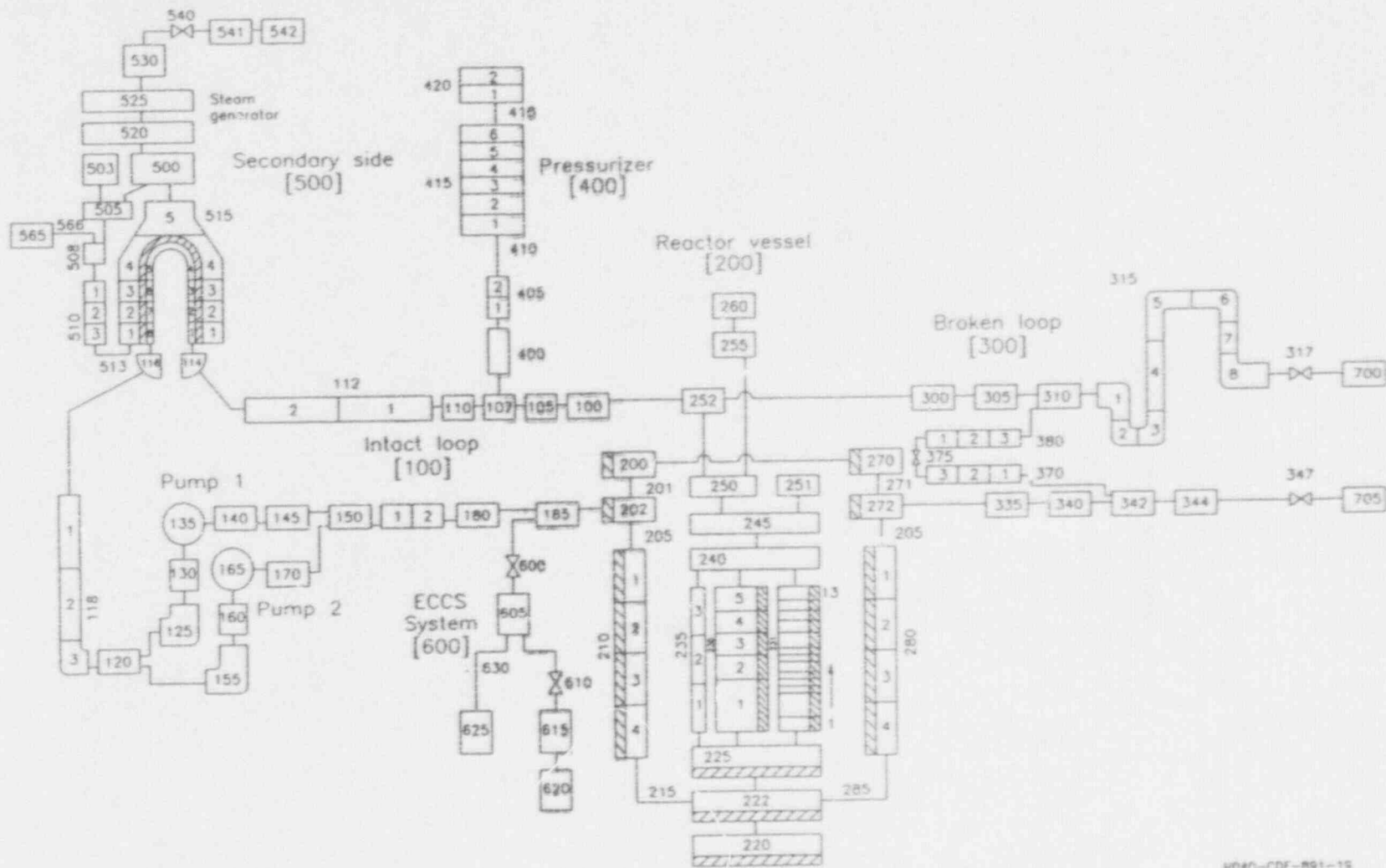
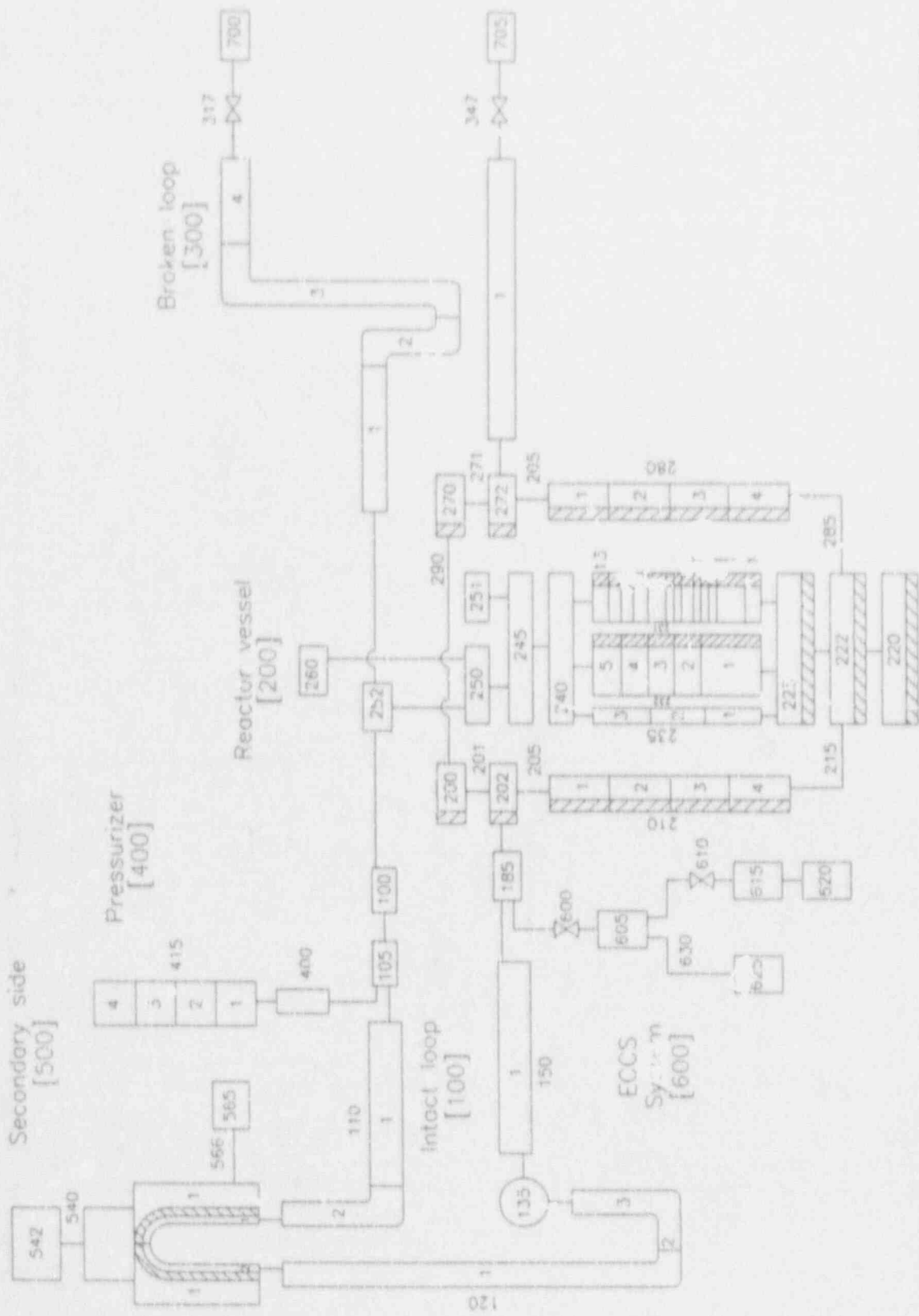
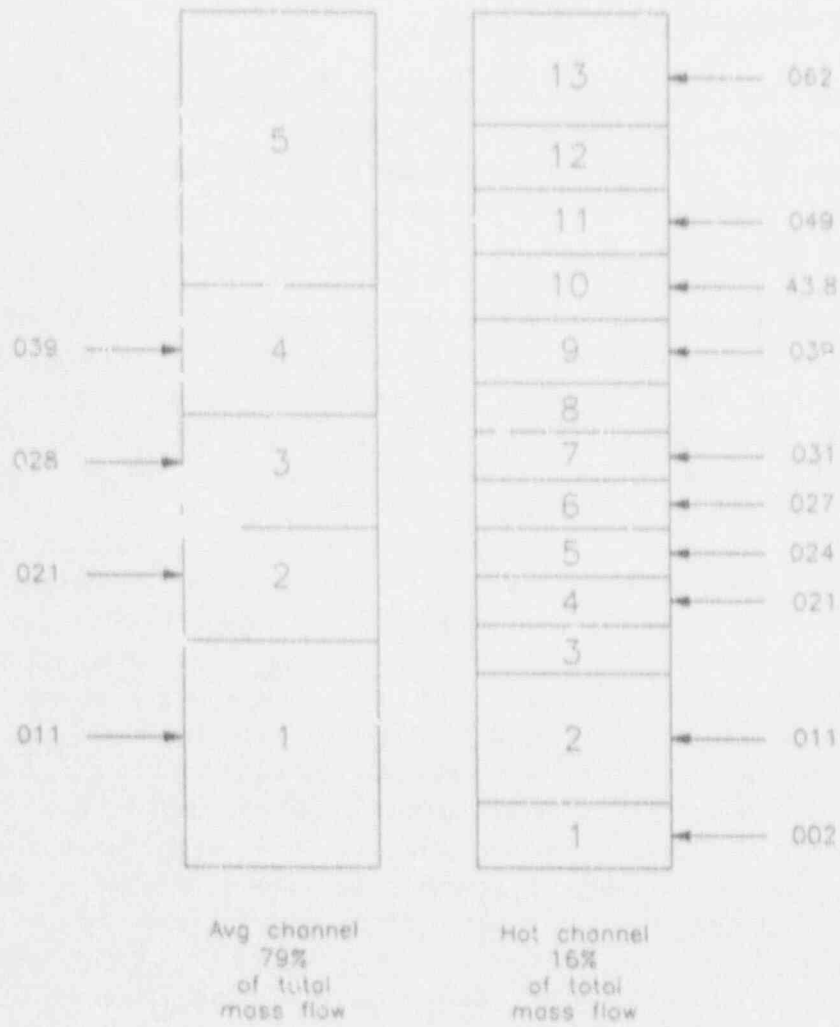


Figure 5-10. Detailed Loss-of-Fluid Test nodalization for large break loss-of-coolant accident analysis.



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Figure 5-11. Simplified nodalization of the Loss-of-Fluid Test system for large break loss-of-coolant accident analysis.



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Figure 5-12. Detail of the nodalization of the Loss-of-Fluid Test core (average and hot channels).



number of junctions and volumes has not always led to a faster calculation. Sometimes, with respect to computing time and because of numerical instabilities, the profit of a much reduced nodalization is rather small.

- For LBLOCAs, the nodalization seems to be important only for the cladding temperatures, where significant differences can be observed for the different nodalizations under investigation.
- For the other parameters, the deviations between the results of the calculations with the different nodalizations under investigation have error bounds of less than  $\pm 20\%$ ; surprisingly, however, the results of runs with less detailed nodalizations usually seem to be closer to the experimental data than the ones with the more detailed basic nodalization scheme.

Work has been done by other researchers to investigate the effect of crossflow junctions in the core and downcomer. Perhaps the earliest report recommending crossflow junctions was summarized by Adams (Adams et al., 1986) based on assessment work done using RELAP5/MOD1. Adams recommended that the downcomer be nodalized as two components with crossflow. He recommended that the downcomer be split one-third and two-thirds, with the larger part associated with the broken loop. Other researchers (Bang et al., 1991; Kao et al., 1988) have used baseline models that included crossflow capability in the vessel downcomer and/or in the core. Kao modeled crossflow in both locations but did not evaluate the effectiveness of such nodalization. Bang began his analysis with a simplified core (i.e., the core was modeled with a PIPE component containing 12 cells, and a downcomer was modeled using two parallel paths with crossflow junctions). This model showed unrealistic downcomer bypass behavior and poor correspondence between the calculated core temperatures and the data. Bang's nodalization studies included an investigation of the effect of removing the crossflow junction couplings in the downcomer below the cold leg elevation and a two-component core section that represented the average and hot portions of the core (the core components were not connected using crossflow junctions). His final recommendations were (a) that the vessel downcomer should not have crossflow junctions for the geometry below the cold leg elevations, and (b) representing the average and hot portions of the core is important in better simulating the core temperature distributions because LBLOCA transient behavior is not uniform.

In summary, since Bang's work is supportive of Lubbesmeyer's approach and since Adam's work was done using an early version of RELAP5, it appears that the best starting point for an LBLOCA analysis is to (a) use a two-component representation for the core if simulation of the high-powered fuel rod behavior is important in meeting the analysis objectives, (b) do not model crossflow in the downcomer, and (c) in general, use a simplified system nodalization if possible.

## 5.2 Unique Features of Babcock & Wilcox Plants

Several design features of Babcock & Wilcox (B&W) plants present special modeling problems. These features and examples of recommended modeling are presented in this section.

## 5.2.1 Reactor Vessel

Two unique features of the B&W reactor vessel require special modeling consideration: the upper plenum region and reactor vessel vent valves. Except for core nodding, Figure 5-10 shows the standard INEL nodalization for a B&W reactor vessel (standard nodding includes six axial core divisions, not three as shown in the figure).

**5.2.1.1 Upper Plenum Region.** The upper plenum region is modeled with components 520, 525, 530, 535, 540, and 545 (see Figure 5-13). The geometry (and hence the nodalization needed) for a B&W reactor vessel upper plenum differs markedly from those in Westinghouse and Combustion Engineering, Inc. (CE) plants that were discussed in Section 5.1.1.

In the B&W reactor vessel upper plenum, parallel flow paths exist for core flow to reach the hot legs. Component 520 combines the main core flow with the core bypass flow. The central region of the upper plenum is confined within a vertical cylindrical baffle. This region is modeled with components 525 and 530. Inside the baffle, flow is directed upward until it reaches the support plate that separates the upper plenum and upper heads. At that elevation, a series of large-diameter holes in the baffle allows the coolant to flow radially outward, then downward through an annular region defined by the baffle on the inside and by the core barrel on the outside. This annular region is modeled with components 540 and 545. The hot leg nozzles (modeled with crossflow junctions 100 and 200) are connected to the annular region at component 545.

Small-diameter holes in the cylindrical baffle centered adjacent to the hot leg nozzles allow a portion of the core flow to pass directly from the inside to the outside of the baffle. This flow path is modeled with the junction between components 525 and 545.

Just above the core, a portion of the flow enters the guide tube pipes that lead to the upper head. The pipes are modeled with component 580 while the upper head is represented by component 550.

A leakage path opened by the slip-fit between the reactor vessel and core barrel assemblies at the hot leg nozzle penetrations is modeled with a junction between components 565 (the downcomer annulus) and 545. Modeling of this junction is described further in Section 5.1.1.

In Figure 5-13, note the accumulators (termed "core flood tanks" in a B&W plant) and the low pressure injection system discharge into the reactor vessel downcomer. In non-B&W reactor designs this system discharges into the cold legs. The reactor vessel internal vent valves are modeled with valve component 536. These valves are described further in the next section.

**5.2.1.2 Reactor Vessel Vent Valves.** The reactor vessel vent valves are unique to B&W plants. These are large-diameter flapper valves that can open outward to allow flow from the upper plenum to the upper annulus of the downcomer (for their location see component 536 in Figure 5-13). Some plants use four valves, others eight. The valves are evenly spaced around the circumference of the core barrel. The valves' purpose is to prevent steam binding from depressing the core level, or from retarding reflood during accident conditions.

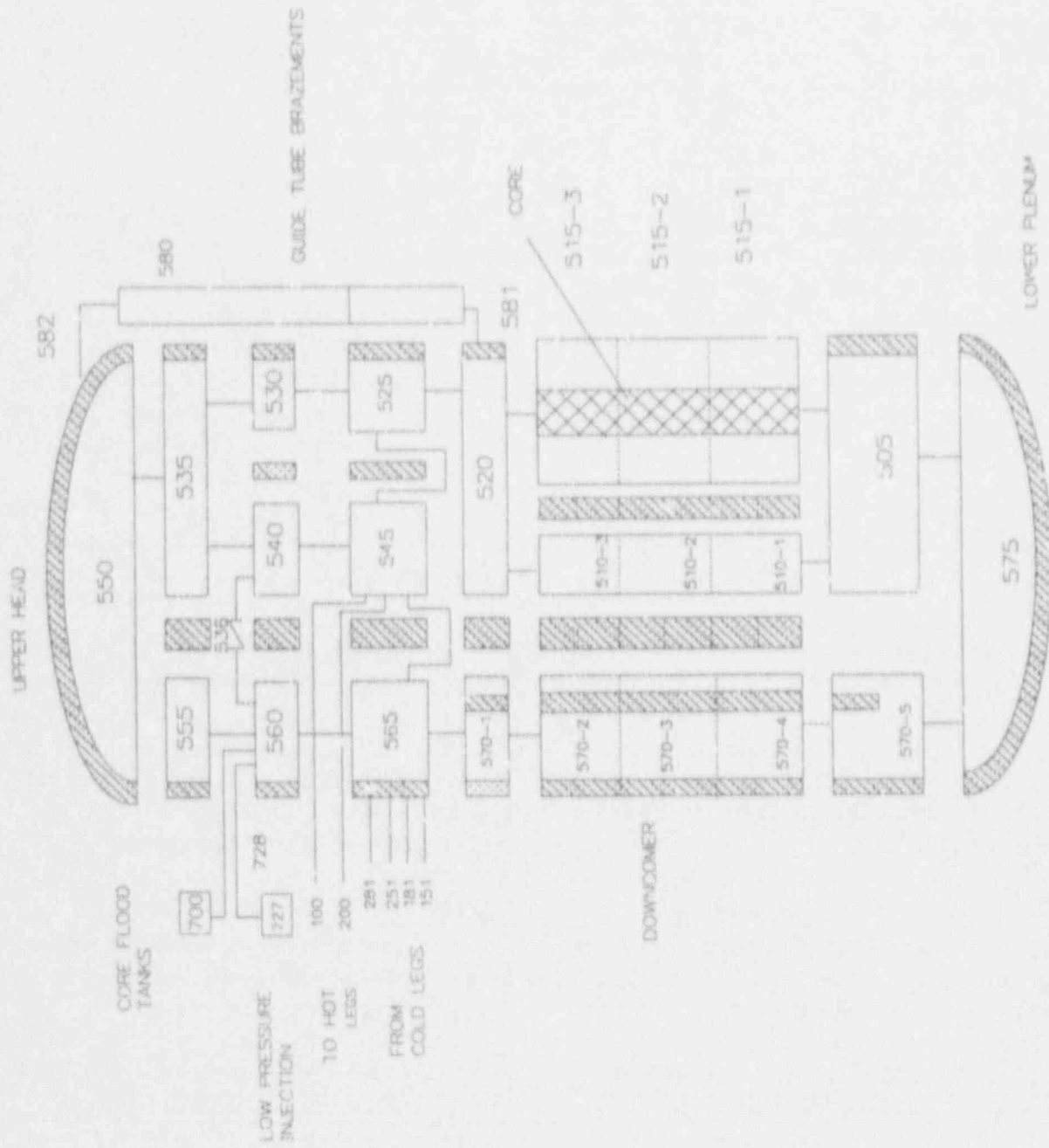


Figure 5-13. Example Babcock & Wilcox reactor vessel nodalization.

The valve flapper is hinged at its top and is held closed by a gravity moment. Static valve tests indicate that for differential pressures below 0.1 psi, the valve is closed. As the differential pressure is increased above 0.1 psi, the valve opens linearly until it is fully opened at a differential pressure of 0.25 psi. Because of these valve characteristics, the vent valves are closed during periods when the reactor coolant pumps are operating and the core flow rate is high. If the reactor coolant pumps are tripped, however, the reduced core flow rate results in a reduced core differential pressure. Experience has shown that if the core flow is due to natural circulation through the coolant loops, then the vent valves will be partially open. Note that the vent valve flow path is parallel to the flow paths from the reactor vessel upper plenum, through the coolant loops, and back to the reactor vessel downcomer. Therefore, if the vent valves are open, there is an internal circulation loop within the reactor vessel that is independent of any loop circulation path. This is a unique thermal-hydraulic feature of B&W plants.

As shown in Figure 5-13, all the vent valves are modeled with a single valve that lumps together the characteristics of the four or eight vent valves. It is recommended that a servo valve component be used; with this valve type, the normalized valve area is specified via a control variable. To determine the valve position, control variables are used to calculate the current differential pressure across the valve and, from the position schedule in the previous paragraph, the current valve normalized area. Because control variables are evaluated on each time step, it is necessary to introduce a time lag to slow the response of the valve model. If a lag is not used, the valve response is virtually immediate and numerical difficulties can be encountered. Such rapid valve "chattering" is not characteristic of the actual valve movement, where the momentum effects of a large metal flapper are significant.

### 5.2.2 Steam Generator

B&W plants employ once-through steam generators (OTSGs) that differ considerably in design from the U-tube steam generators (UTSGs) employed in CE and Westinghouse plants. The OTSG is a counterflow heat exchanger that employs straight tubes. The standard INEL OTSG nodalization is shown in Figure 5-14. Components 116 and 125, represent the OTSG inlet and outlet plena, respectively. Single-sided heat structures represent the significant metal structures (such as the steam generator heads and the tubesheets). Reactor coolant flows downward through the insides of the tubes; 8-cell pipes 120 and 121 represent the tube primaries. Pipe 120 represents 90% of the OTSG tubes, pipe 121 represents the other 10% (the reason for separating the tubes in this manner is discussed below). Two-sided heat structures model the tube walls.

On the secondary side, the downcomer region is modeled with 4-cell pipe 305. Main feedwater enters the downcomer at the upper end of this component. Single-sided heat structures represent the steam generator shell and the vertical baffle that separates the boiler and downcomer regions. Branch 306 represents the region at the lower tubesheet, where the flow changes direction from downward to upward.

The boiler region is separated into two parallel flow paths, representing 90% and 10% of the flow area. The paths are connected by crossflow junctions. Components 310 through 323 represent the 90% region while components 360 through 372 represent the 10% region. The

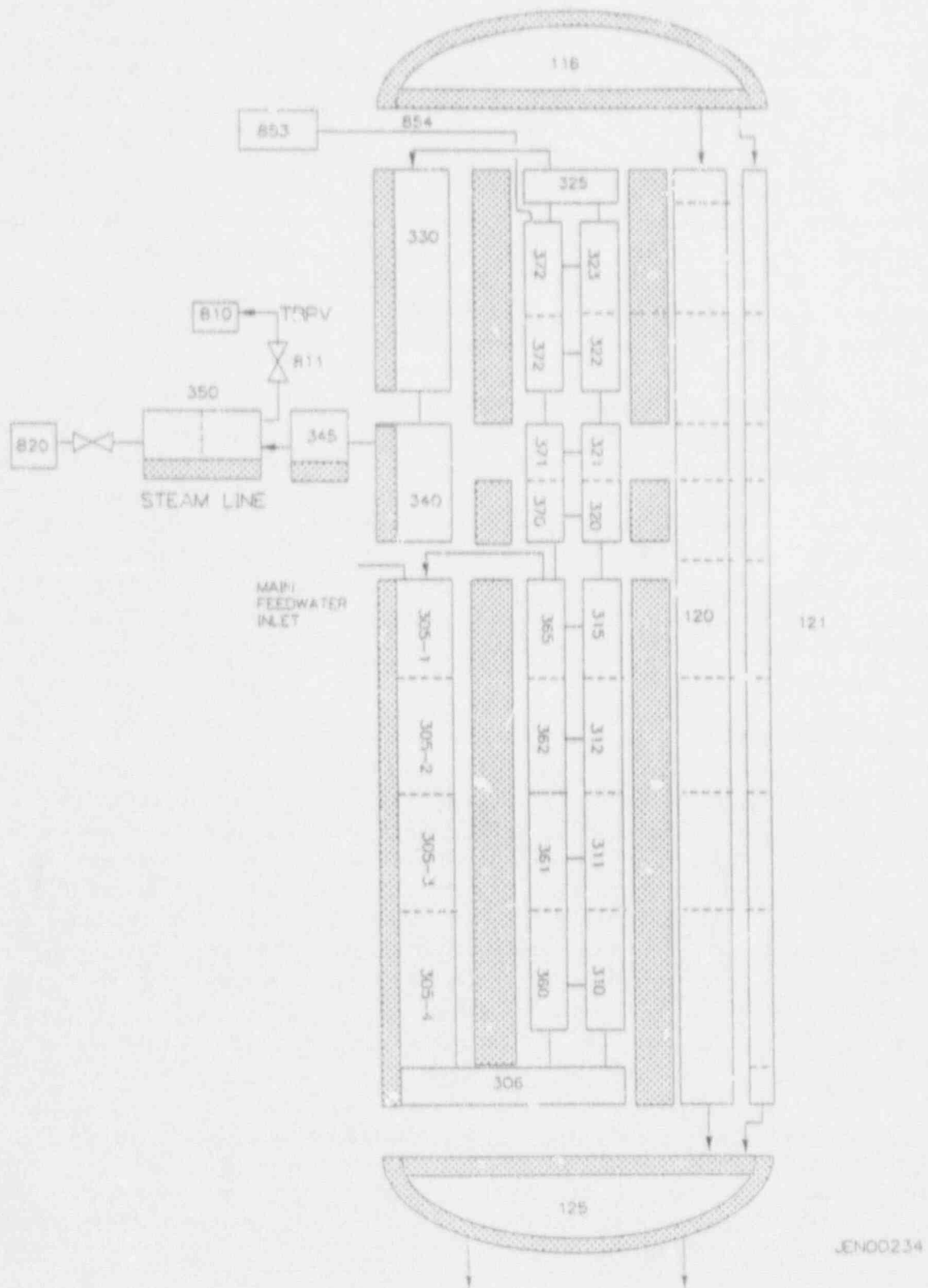


Figure 5-14. Example Babcock & Wilcox steam generator nodalization.



split boiler region model is recommended to simulate phenomena during periods of emergency feedwater injection. This injection enters the boiler around the circumference of the boiler, near the upper tubesheet (junction 854 in the model) and is directed radially inward, into the tube bundle. Because the OTSG employs over 15,000 tubes, the emergency feedwater wets only a small portion of the tubes around the periphery of the tube bundle. As the emergency feedwater falls downward, it encounters the tube support plates (there are 17 in the OTSG) that tend to spread the injection flow further into the tube bundle. The split boiler nodalization represents a compromise modeling scheme for simulating this behavior. An initial 10% bundle penetration is expected, and the crossflow connections to the 90% region allow simulation of the inward spreading.

At the top of the boiler region, flows from the parallel boiler channels are combined in branch 325 before exiting the steam generator through a steam annulus, modeled with components 330 and 340.

Modeling the behavior of an OTSG is perhaps the most difficult of nuclear thermal-hydraulic system code problems encountered. The difficulty arises for two reasons. First, a complete spectrum of heat transfer phenomena is experienced between the tube wall and the secondary fluid. At the bottom of the tubes, heat transfer is to subcooled liquid. As the flow progresses up the tubes, the liquid is then saturated and boiled away. To preheat the feedwater, a portion of the steam flow is bled into the downcomer through an aspirator near mid-boiler (modeled with the junction between components 365 and 305 in Figure 5-14). Further up the tubes, any remaining droplets are vaporized and the steam is significantly superheated. Second, the OTSG heat removal rate is very sensitive to the secondary-side liquid level. As the level increases, more of the tube surface area experiences effective heat transfer (e.g., boiling) rather than ineffective heat transfer (e.g., convection to steam). Moreover, the sensitivity of OTSG heat removal to level is present during normal operation, while for UTSGs this is a concern only during accidents that involve an extreme depletion of secondary liquid.

The OTSG steam generator nodalization shown in Figure 5-14 has proven adequate for simulating normal operation. The difficulty in obtaining a satisfactory OTSG simulation described above is partly nodalization dependent. Nodalization is by nature discrete, and this causes the steam generator heat removal in the model to be even more sensitive to the secondary level than in the prototype. In the model, as the level moves across cell boundaries, discrete jumps in overall heat transfer are encountered. These changes often cause the model to become unstable, oscillating between two solutions at two different secondary levels. Moving to finer axial noding may remedy the oscillation, however the proximity of the liquid level to cell boundaries often is more important than cell size.

### 5.2.3 Hot Leg

The hot leg geometry of B&W plants differs markedly from that of Westinghouse and CE plants. The B&W hot leg includes a tall vertical section, leading to an inverted U-bend. Figure 5-15 shows the standard INEL nodalization for the hot legs of B&W plants. Heat structures are used to represent the piping walls.

#### 5.2.4 Cold Leg

B&W coolant loop design includes two cold legs per steam generator. Because this design feature is the same as for CE plants, the reader is referred to Section 5.3 for additional modeling information. The standard INEL nodalization for the cold legs of B&W plants is shown in Figure 5-15. Heat structures are used to represent the piping walls.

#### 5.2.5 Plant Control Systems

The control systems included for a given analysis are dependent on the transient of interest. Because of the integrated nature of the B&W plant control systems, the investigator may find that many interactions within the control system must be considered. Moreover, the B&W control system is proprietary. Thus, the ultimate decision concerning what portion of the system must be included is dependent on the transient of interest and whether or not B&W will give the investigator the necessary information. Regardless, past experience at the INEL has indicated that the components contained within RELAP5/MOD3 are adequate to simulate the control system's interactions.

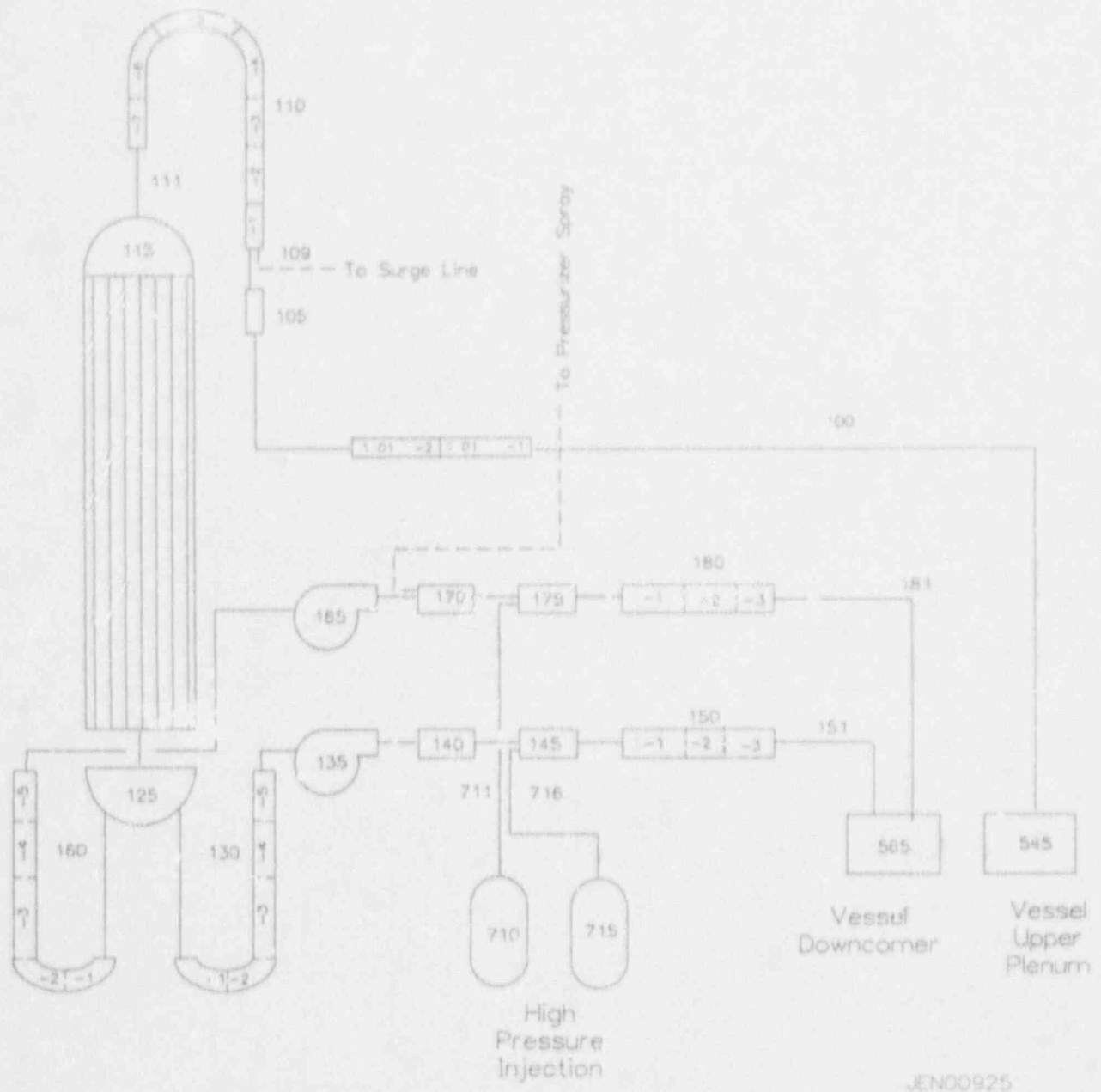
To assist the user in applying the RELAP5/MOD3 control system components to B&W applications, the following paragraphs outline an application of the RELAP5 control blocks to the Davis-Besse Plant when a loss of feedwater uncertainty analysis was undertaken (Davis, 1987).

Many of the plant control systems were represented. These control systems include the integrated control system (ICS), pressurizer pressure control system, anticipatory reactor trip system (ARTS), and steam and feed rupture control system (SFRCS). These control systems are described in greater detail below.

The RELAP5/MOD2 model of the Davis-Besse ICS represents the following subsystems: unit load demand development subsystem, integrated master subsystem, steam generator feedwater control subsystem, and the reactor control subsystem. Figure 5-16 is a schematic of the ICS organization and presents an overview of the ICS functions. The borate control subsystem and the non-nuclear instrumentation system are not represented. The ICS model is based on information obtained from B&W and Davis-Besse personnel, plant calibration data, detailed schematics of the subsystems, analog and digital logic drawings, and Bailey Meter Company detailed descriptions of the individual modules.

The ICS modules and relays were modeled individually to provide the greatest amount of flexibility for future analysis requirements. Additional control variables were included in the model to allow the analyst the ability to impose false signals during a calculation. For example, a steam generator level signal can be failed to zero interactively to simulate a failed level transducer. Display parameters and display options available to the operator are also available to the analyst during interactive execution.

The RELAP5/MOD2 kinetics package is not used in the Davis-Besse model. Consequently, reactor control rod positioning is not directly coupled to the reactor power. Instead, the reactor power is controlled by general table reference. Reactor kinetics can be incorporated at a later date, as the need arises.



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Figure 5-15. Example Babcock & Wilcox coolant loop nodalization.

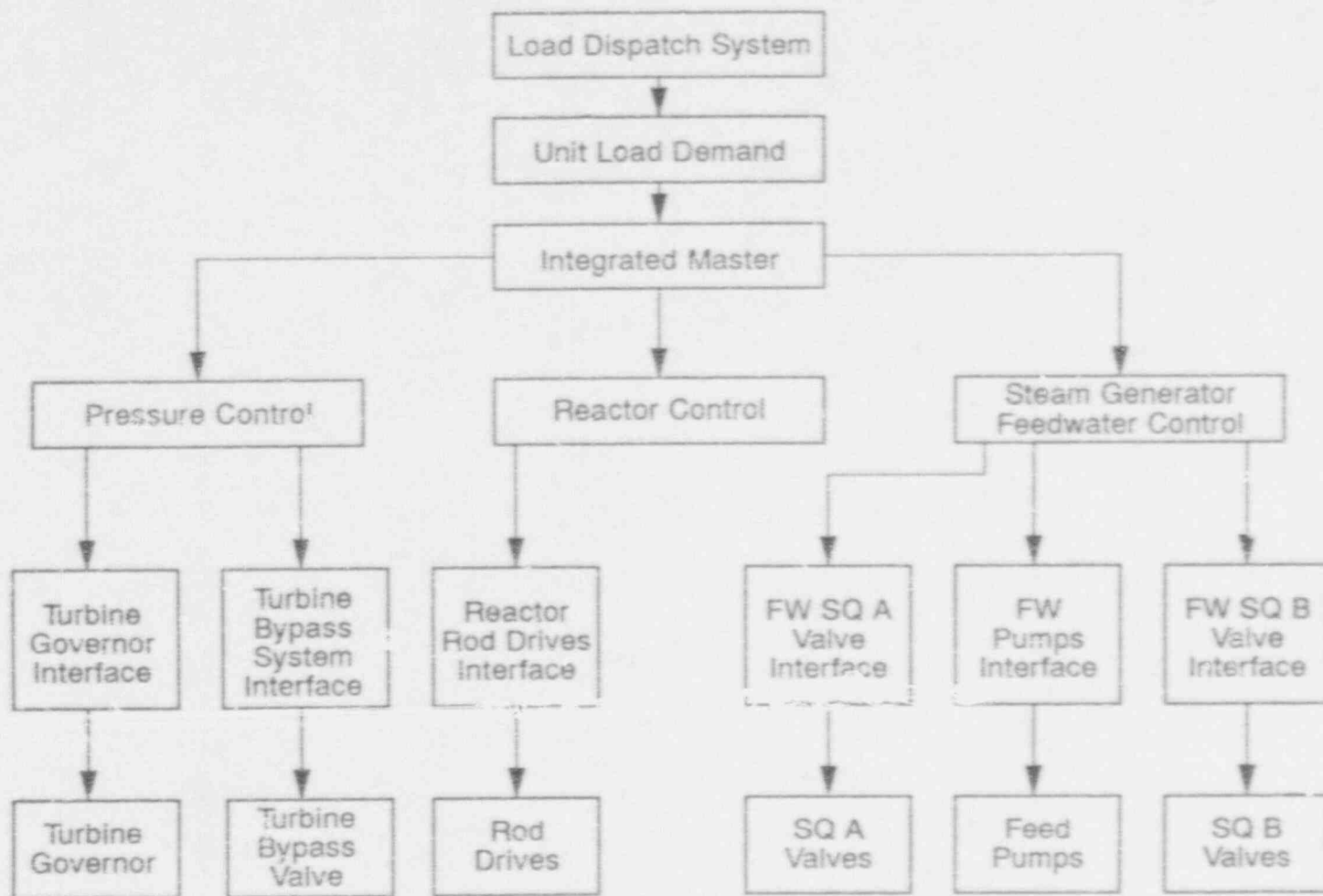


Figure 5-16. Babcock & Wilcox integrated control system organization.

The pressurizer pressure control system was modeled through the representation of pressurizer heaters and spray. Design data on the pressurizer level control system were not available during the development of the model. Instead, a simple logic was developed that controlled the net makeup into the reactor coolant system based on the pressurizer level. The net makeup represented the combination of makeup and letdown, with the net flow added to the A1 cold leg pump discharge. In the plant, letdown is taken from the B1 cold leg pump suction, but the model approximation is thought to be adequate for most applications. The capability to model zero, one, or two makeup pumps and minimum, normal, or maximum letdown, in any combination, was developed.

The model represents the ARTS and SFRCS. Reactor trip is modeled based on high power, high reactor pressure or temperature, power-to-flow ratio, reactor pressure versus temperature, RCP trip, turbine trip, SFRCS actuation, or manual trip. SFRCS is actuated based on low steam pressure, low feedline differential pressure, low or high OTSG level, or reactor coolant pump trip. The model determines the correct alignment of AFW based on the type of SFRCS actuation. In event of a rupture of the steam or feed lines, SFRCS isolates the OTSGs and aligns AFW into the unaffected OTSG.

### 5.3 Unique Features of Combustion Engineering, Inc. Plants

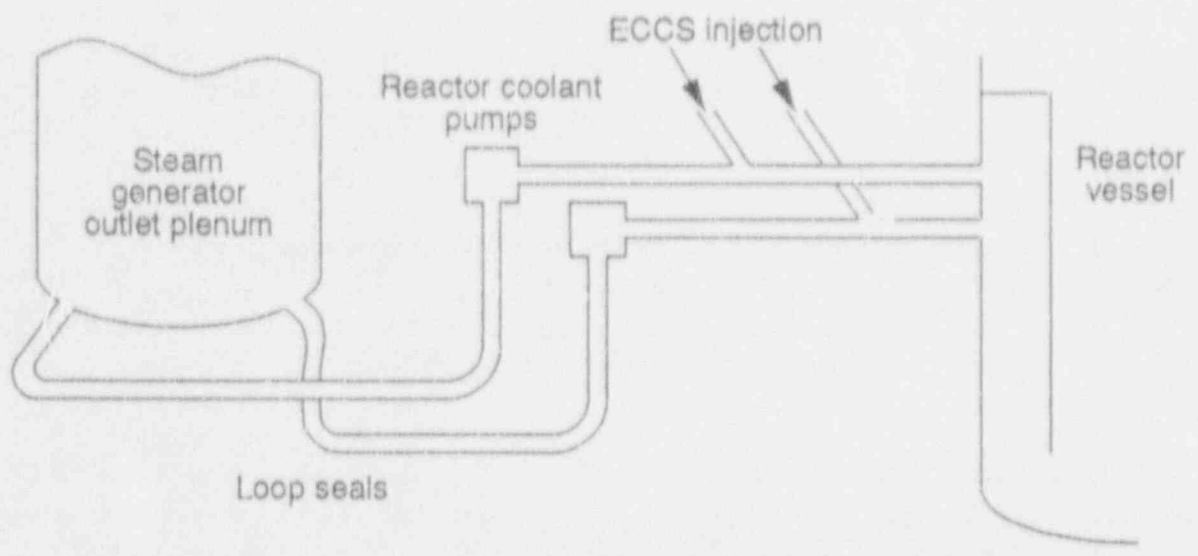
CE plants are quite similar to Westinghouse plants. Therefore, the structure of the example plant model discussed in Section 5.1 is generally applicable to CE plants.

From a RELAP5 modeling perspective, there is only one significant difference between Westinghouse and CE plants: each coolant loop in the CE plants includes two cold legs rather than one. This difference is accounted for by modeling both cold legs from the steam generator outlet plenums to the reactor vessel. The Westinghouse plant cold leg nodalization scheme shown in Figure 5-2 is also recommended for each of the cold legs in a CE plant coolant loop.

Since the two cold legs in a CE plant are virtually identical the modeler may consider combining them into a single cold leg for economy. A technique for lumping identical parallel flow paths is described in Section 5.5. However, to retain model generality, it is recommended that the two cold legs not be lumped together. In situations where forced and natural circulation through the cold legs is lost (e.g., during a LOCA when the reactor coolant pumps are tripped and the loops are partially drained) asymmetric behavior of the two same-loop cold legs can occur. Depending on the simulation, this asymmetry can be important.

Figure 5-17 illustrates the possibility of same-loop cold leg asymmetry. To show detail, the elevations of the two cold legs have been offset slightly in the figure; in both the plant and the model, cold leg elevations are identical. Consider a transient where the total coolant loop circulation has been lost and the hot leg flow has been terminated. Emergency core cooling system (ECCS) flow is injected into both cold legs in each coolant loop of a CE plant. Under these conditions, the steam generator outlet plenums, the cold legs, and the reactor vessel downcomer contain single-phase liquid. As the ECCS injection continues, a thermal distribution appears: Liquid between the ECCS injection site and reactor vessel becomes cooler as the region





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**Figure 5-17.** Cold leg recirculation in through same-loop cold legs in a Combustion Engineering, Inc. plant.

is flushed by the cold injection flow while the remaining liquid is not so cooled. This effect, by itself, does not cause asymmetry between the same-loop cold legs. However, minor differences between the two cold legs (leading to different injection rates) and fluid mixing effects can cause an asymmetric flow pattern to develop. From these effects, fluid in the pump-to-ECCS site regions of the two cold legs may be expected to cool at different rates. When the cooling front reaches the reactor coolant pump, a flow instability is set up due to buoyancy effects. The cold fluid backflowing into the pump will reside above warmer fluid in the vertical cold leg piping from the loop seal to the pump. As a result, the cold leg in which this behavior is first experienced will start to flow in reverse while the other cold leg will start to flow in the normal direction.

Once initiated, this same-loop cold leg recirculation will tend to continue. The reverse-flowing cold leg continually sweeps the cold ECCS injection fluid into its pump suction region. This cold fluid is mixed with the warmer fluid in the steam generator outlet plenum and the warmed mixture enters the pump suction region of the forward-flowing cold leg. The difference in fluid densities between the two pump suction vertical regions thus provides a sustained buoyancy driving force for a recirculation flow between the two same-loop cold legs.

The same-loop cold leg recirculation pattern has been observed in several past RELAP5 analyses. Depending on the simulation, this effect can be significant. For example, if the temperature of fluid in the top of the reactor vessel downcomer is pertinent, the temperature is much higher if the recirculation is present than if it is not. Therefore, to retain model generality, it is recommended that both cold legs on each loop be included when modeling CE plants.

## 5.4 Notes on Modeling Pressurized Water Reactor Metal Structures

The base case example application in Section 5.1 provides detailed guidance on modeling metal structures within each of the PWR components. This guidance generally recommends that all metal structures that interact with the primary and secondary system coolant be included in a model. A frequent source of analysis error involves failing to follow this recommendation.

Developing input for heat structures can be tedious and requires another review of the component prints to obtain wall thicknesses, materials, etc. It is therefore tempting to include "active" heat structures but exclude "passive" heat structures from a model. For example, a PWR model with only active structures might include the core fuel rods and steam generator tubes (i.e., only the heat structures needed for simulating the plant steady-state heat balance are modeled). The resulting model often is not adequate for simulating PWR behavior. During a transient simulation, the "passive" metal structures (i.e., those not involved in the steady-state heat balance) can provide significant heat sources or sinks to the primary and secondary fluid systems. It is therefore highly recommended that the passive structures be included in a PWR model. As motivation to follow this recommendation, the analyst should consider that the heat stored in a PWR's passive heat structures (piping walls, component internals, and external shells) is approximately half that stored in the combined primary and secondary system coolants.

Another potential heat structure modeling difficulty regards initialization of heat structure temperatures in calculations that do not begin from a well-documented plant condition. In simulations that begin from PWR full-power steady-state conditions, the heat structures are adequately initialized by allowing the code to determine the thermal distributions within the

structures that are consistent with the internal heat sources and the surface heat transfer rates. However, consider the example of starting a simulation at the beginning of reflood following a PWR large break LOCA. The heat structure thermal distributions at the beginning of core reflood will be significantly different than those at full power operation. A common modeling error is to overlook this difference and fail to re-initialize the heat structures at the proper conditions for the beginning of reflood. Often, the modeler recognizes the need to re-initialize the active heat structures, such as the fuel rods, but fails to re-initialize the passive heat structures.

Finally, the PWR modeler should consider the significance of environmental heat loss from the outer surfaces of the primary coolant system. The example PWR application provided in Section 5.1 neglects this heat loss by assuming adiabatic boundaries on the outer surfaces of the piping and shell heat structures. For PWRs, the environmental heat loss to containment during normal operation is about 8 MW, or about 0.3% of the core thermal power. Neglecting this heat loss generally does not significantly affect the simulation of most accident scenarios, even when the core power is solely due to decay heat. However, the modeler should consider whether this assumption remains appropriate for transient simulations that include (a) very low decay heat levels, such as would be present long after a reactor trip, or (b) model regions where localized heat losses may be important when compared with the coolant energy flows. For a sub-scale experimental facility, environmental heat losses generally should be modeled because for such facilities the ratio of these losses to the core power typically is much higher than for the full-size plants.

## 5.5 Lumping Coolant Loops

A technique with potential to minimize model complexity, assembly time, and computational time is to lump two or more PWR coolant loops together. However, individual loop modeling is preferred because it (a) maintains model generality, and (b) is not necessary to determine early in the modeling process if lumping loops is appropriate. If a modeler elects to lump coolant loops, the following discussion provides guidance for doing so. In this discussion, it is assumed that two loops will be lumped together into one in the model; a similar logic is used for lumping three loops together.

When lumping two coolant loops together, the lumped loop should be scaled up by a factor of two but remain hydraulically similar to the single loop. After scaling, the lumped loop will have twice the fluid volume, fluid flow area, heat structure metal volume, heat structure surface area, and mass flow rate as the single loop. Hydraulic similarity calls for the single and lumped loops to have the same flow velocities, pressure drops, and wall heat transfer coefficients. Table 5-1 provides general guidance for lumping together two identical loops. The table shows what modifications need be performed to the input data of an existing single-loop model in order for them to represent two loops.

Table 5-1. Guidance for converting a single-loop model to a two-loop model.

Parameter	Lumped Loop vs. Single Loop
<b>Hydrodynamic Volumes</b>	
Cell flow area	Twice
Cell length	Same
Cell volume	Twice
Azimuth angle	Same
Inclination angle	Same
Elevation change	Same
Wall roughness	Same
Hydraulic diameter	Same <sup>a</sup>
Volume control flags	Same
Initial cell conditions	Same
<b>Hydrodynamic Junctions</b>	
Connection codes	Same
Junction flow area	Twice
Forward and reverse loss coefficients	Same
Junction control flags	Same
Junction hydraulic diameter	Same <sup>a</sup>
Countercurrent flow limiting parameters	Same
Initial velocities	Same
Initial mass flow rates	Twice
<b>Heat Structures</b>	
Numbers of axial heat structures	Same
Number of mesh points and geometry	Same
Steady-state initialization flag	Same
Left boundary coordinate	Same
Reflood flags	Same
Boundary volume indicator	Same
Maximum axial intervals	Same
Mesh location and format flags	Same
Mesh intervals and coordinates	Same
Composition data	Same
Relative source values	Same
Initial temperature data	Same
Boundary volumes, increments, and condition types	Same
Surface area codes	Same
Surface area correction factors	Twice

Table 5-1. (continued).

Parameter	Lumped Loop vs. Single Loop
Heat Structures (contd.)	
Source type	Same
Internal source and direct heating multipliers	Twice
Heated equivalent diameter	Same <sup>a</sup>

a. Same unless zero (default value) is used in the single-loop model, in which case the actual single-loop number should be calculated and used.

## 5.6 Model Assembly Methods

In general, the model should match the physical system as closely as possible. To follow this philosophy, a very fine nodalization will be needed so that minor features of each fluid region within the plant can be represented. However, a very fine nodalization is not economic. The example PWR nodalizations in Sections 5.1, 5.2, and 5.3 represent compromises between calculational fidelity and economy. These compromises have evolved over years of experience in applying RELAP5 to a spectrum of plant accidents and transients at the INEL and elsewhere.

To assemble a model, a set of information will be needed. The best sources of information are the complete drawings of the plant and documentation that describes its control and operation.

For hydrodynamic cells, it is necessary to input flow area, volume, length, inclination angle, elevation change, wall roughness, hydraulic diameter, volume control flags, and initial conditions. Unlike some thermal-hydraulic system codes, with RELAP5 it is necessary for the cell flow area, volume, and length to be mathematically consistent. This requirement causes the modeler to compromise one of these input parameters in situations where the flow area within a cell changes as a function of position within the cell. Often, a satisfactory compromise is possible by considering which of the three parameters is least significant, and the effect on the problem because of the error introduced. If a compromise cannot be made because it would significantly alter the problem, then the modeler should make the nodalization fine enough so that behavior may be better simulated.

The vertical angle determines the applicable flow map, horizontal or vertical. With RELAP5/MOD3, the flow map switch is made at an angle of 45°; this is a departure from previous code versions where the switch was made at 15°. It is important that the actual elevation change be input. The code requires the elevation change to be equal to or less than that implied



by the cell length and vertical angle. If this requirement causes difficulty, the modeler should consider artificially revising the vertical angle since this revision has no effect on the problem unless the flow map switch point is crossed.

The wall roughness input should be consistent with the pipe material. In most PWR applications, good results are obtained with a commercial steel roughness of 0.00015 ft (see Crane, 1980). An exception is to use a drawn tubing roughness of 0.000005 ft (see Crane, 1980) for the inner and outer surfaces of steam generator tubes. A hydraulic diameter should be calculated as four times the flow area divided by the wetted perimeter. This calculation is straightforward unless the geometry changes as a function of the length within the cell. In cases where the flow area changes continuously with length, the average flow area and hydraulic diameter may be used. In cases where the flow area changes in steps, length-weighted average flow area and hydraulic diameter may be used. In these situations, the modeler should consider the error introduced and use a finer nodalization if the error is not acceptable.

Volume control options should be based on the recommendations in Section 3.3.1. Volume initial conditions should be input based on the recommendations in Section 3.3.3.1. For most PWR system models, the model will be initialized at full or reduced power conditions. While the modeler may have some knowledge of the desired conditions, it is not necessary to precisely input them. Instead, only crude approximations of these conditions are needed because the actual steady-state conditions will later be calculated with the code (see Section 5.7).

For hydrodynamic junctions, it is necessary to input the connection codes, junction flow area, forward and reverse flow loss coefficients, junction control options, and junction initial conditions.

The junction connection codes specify the manner in which the hydrodynamic cells are connected. It is important that the modeler understands the conventions used for specifying the connections (see Section 5.6.3). The junction flow area does not need to be consistent with the flow areas of its adjacent hydrodynamic cells. However, the modeler should understand that the junction flow area should be consistent with any user-input flow loss coefficients. Generally, good pressure drop simulations have been obtained with pipe bend and fitting losses estimated using the methods in *Flow of Fluids through Valves and Fittings* (Crane, 1980). Another useful source of bend and fitting loss information is the *Aerospace Fluid Component Design Handbook* (Rocket Propulsion Laboratory, 1970). An exhaustive catalog of flow losses in complex geometries is found in the *Handbook of Hydraulic Resistance, Coefficients of Local Resistance and of Friction* (Idel'chik, 1966). Junction control options should be input based on the recommendations in Section 3.3.2 and junction initial conditions should be input as described in Section 3.3.3.2. As with the hydrodynamic cells, it is generally not necessary to precisely specify the junction initial conditions in a PWR system model.

For heat structures, it is necessary to input information describing the heat structure cross-sectional geometry, surface area, and sources and sinks. Heat structure input requirements are summarized in Section 4.7 and guidance for modeling heat structures is provided in Sections 3.2.2, 3.3.3.3, and 3.3.4.3. Additional information needed to model PWR heat structures typically includes wall thickness, materials, and data regarding the magnitude and distribution of heat sources and sinks.

To model control systems, it is necessary to obtain or develop block diagrams describing their function. Example PWR control systems are described in Sections 5.1.7 and 5.2.5. The RELAP5 control variable component is described in Section 4.10. The modeler is cautioned that plant documentation summarizing control systems is often incomplete or outdated. As a result, the actual current PWR control system setpoints and gains should be obtained and used.

## 5.7 Obtaining Satisfactory Steady-State Conditions

Once the PWR model has been assembled as described in the previous section, it is necessary to obtain a satisfactory steady-state model condition to initiate transient calculations. Typically, a steady-state condition representing PWR full-power operation is calculated first. This calculation allows an overall verification that the model accurately represents the plant. For operating plants, measured full-power plant parameters are available.

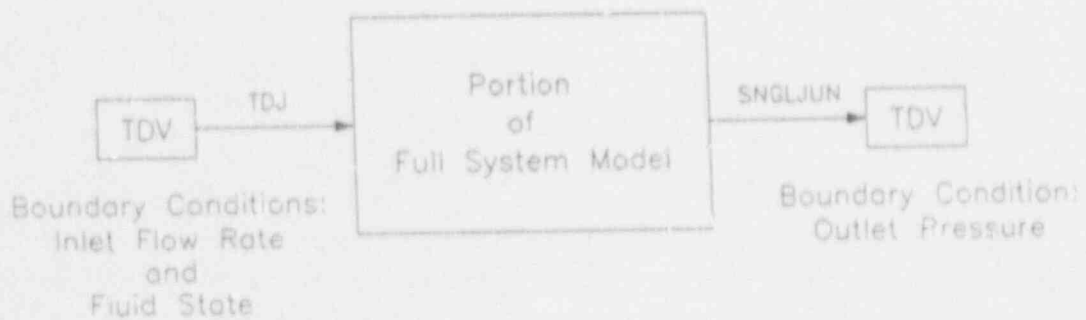
The effort required to obtain a satisfactory steady-state system model calculation varies widely, and primarily depends on two factors: (a) the care and foresight with which the modeler has assembled the model, and (b) the willingness of the modeler to approach the task using a methodical series of steps that simplifies the process. If, during the assembly process, the modeler considers nodalization and assumptions, takes care when entering and checking the model input, and is willing to obtain satisfactory steady-state calculations for individual plant components, then success at attaining a system model steady-state calculation is ensured with only a modest effort. On the other hand, improper nodalization and assumptions, carelessness when entering or checking input data, and attempting to steady a full model without first steadying its components often lead to an expensive, prolonged effort.

The following sections describe a general method for obtaining steady conditions for a portion of a model, followed by a discussion of a step-by-step method application for obtaining a full power steady-state for the example PWR model in Section 5.1.

### 5.7.1 General Method

Figure 5-18 illustrates a general method of obtaining a steady-state calculation for a portion of a system model. For example, the model portion may be one steam generator, a reactor vessel, a hot leg, a cold leg, or a combination of these. The method involves imposing inlet flow and outlet pressure boundary conditions on manageable sections of the overall system model for the purpose of individually checking each section's performance before linking them together.

The inlet flow boundary condition is specified by connecting time-dependent volume (TMDPVOL) and time-dependent junction (TMDPJUN) components at the upstream end of the model. A TMDPVOL specifies fluid condition (pressure, temperature, or internal energies of the phases, and void fraction or quality). A TMDPJUN specifies a flow velocity or mass flow rate. As described in Sections 5.6.2 and 5.6.4, the "time-dependent" adjective is a misnomer because the boundary conditions may be specified as functions of virtually any calculated variable, not just time. However, for our purpose here, the inlet TMDPVOL and TMDPJUN will specify the constant fluid conditions and constant flow rate that are associated with the steady-state operation.



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Figure 5-18. General method for driving a portion of a full system model to steady conditions.

The outlet pressure boundary condition is specified by connecting the downstream end of the model to a TMDPVOL component through a normal RELAP5 junction (such as a single junction, valve junction, or branch junction). The outlet TMDPVOL specifies a constant pressure, representing the steady-state conditions.

The arrangement shown in Figure 5-18 often is a source of confusion to beginning modelers. The inlet TMDPVOL is used only to specify the conditions of the fluid that the inlet TMDPJUN injects into the model. Therefore, changing the pressure of the inlet TMDPJUN affects the enthalpy of the inlet fluid but does not otherwise affect the pressure solution within the remainder of the model. The flow boundary condition specified at the inlet TMDPJUN effectively isolates the inlet TMDPVOL from the model. In other words, the TMDPJUN forces the inlet flow, regardless of the pressure difference across it. The pressure distribution within the model is defined by the downstream pressure (specified in the outlet TMDPVOL) and the flow behavior and losses generated within the model when the desired flow is passing through it. Thus, it is important to couple the model to the outlet TMDPVOL using a normal RELAP5 junction so that the differential pressure across it may be accurately calculated.

The diagram shown in Figure 5-18 represents only the simplest of modeling situations, such as coolant flow through a piping system with no heat addition or loss and no flow addition or leakage. This method would, for example, be adequate for obtaining a steady-state calculation for PWR hot leg piping. The method is extended to these more complex situations (examples to be shown shortly) through the addition of heat or flow sources, as appropriate.

The method to obtain an acceptable steady-state condition for a portion of the model is to specify the inlet flow and outlet pressure boundary conditions (and in some instances heat and flow sources and sinks), execute the model portion, and compare the calculated model conditions with the desired conditions. In the example model shown in Figure 5-18, the calculated condition of interest is the pressure at the inlet of the model. If the modeler has carefully modeled the physical system, then the pressure drop across the model will closely match the actual pressure drop.

If the calculated conditions are in acceptable agreement with the measured or specified conditions, then the modeling approach is verified. However, if the agreement is not acceptable, then either (a) the measured data are not correct, or (b) one or more aspects of the model are incorrect. In most instances, the source of disagreement is found to be modeling error, rather than measurement error. When disagreements arise, the modeler should first review the appropriateness of the modeling assumptions and the model implementation.

In the example model, disagreement would be caused by failure to match the pressure drop across the model. First, the modeled flow rate and fluid density would be double-checked for accuracy. If, for example, the calculated pressure drop is too large, then too much flow loss has been included in the model. Flow losses result from a combination of distributed wall friction and lumped flow resistances. Generally, RELAP5 adequately represents wall friction pressure drop if the appropriate wall roughnesses, hydraulic diameters and velocities are input. Therefore, the modeler should double-check the implementation of these parameters. Next, the input lumped flow losses should be checked. Often, the actual lumped losses are uncertain because of unique geometries and this gives the modeler license to adjust the input loss coefficients. Adjusting a

lumped loss coefficient within the range of its reasonable uncertainty is justified if the change allows the model to come into agreement with measured data. Experience has shown that this step typically is successful. If it is not, then it is an indication of modeling error or misinterpretation of the measured data.

To demonstrate the application of the steady-state methods, consider the process of obtaining a full power operation condition for the example Westinghouse plant described in Section 5.1. The following sections describe this process in a step-by-step manner.

### 5.7.2 Step 1—Reactor Vessel

Figure 5-1 shows the nodalization of the reactor vessel model. The model performance success criteria include matching measured data for core power, hot and cold leg flow rates, hot and cold leg fluid temperatures, the reactor vessel differential pressure, and the distribution of flow within the various reactor vessel internal flow paths. Section 5.1.1 provides additional discussion regarding reactor vessel initialization.

The reactor vessel model is exercised by applying a flow boundary condition for the inlet mass flow rate, a temperature boundary condition for the inlet fluid temperature, a pressure boundary condition for the outlet pressure, and a heat source boundary condition for the core power. This combination of boundary conditions ensures that the calculated total reactor vessel flow rate, hot leg pressure, and hot leg fluid temperature will be correct.

The first calculated solution for the reactor vessel likely will be quite close to the desired conditions. Minor adjustments of the lumped flow loss coefficients may be necessary to obtain the desired reactor vessel internal flow splits. These adjustments should be implemented in locations where the flow loss is not well known. The reactor vessel internal flow pattern solution is based on many individual flow paths in series and parallel configurations. Therefore, the adjustment process proves to be iterative. To minimize the effort, it is recommended that adjustments begin with paths with the highest flow rates and proceed toward paths with the lowest flow rates.

Experience has shown that the flow losses at the upper and lower core support plates and within the core bypass region are often not well known. In practice, adjusting the loss coefficients representing these features may be justified. Additionally, the applicable flow areas and losses of the leakage paths (the flow through component 100, and the flow from component 102 to component 120) are even less well known. For these paths, an arbitrary flow area is selected and loss coefficients are adjusted as needed to obtain the desired flow rate.

### 5.7.3 Step 2—Steam Generator and Steam Lines

Figures 5-3 and 5-5, respectively, show the nodalization of the steam generator and steam lines. The model performance success criteria include matching measured data for primary side flow rate, hot and cold leg temperatures, feedwater and steam flow rates, feedwater temperature, and the distribution of flow within the steam generator secondary side.



The steam generator model is checked out by applying boundary conditions for the hot leg flow rate, hot leg fluid temperature, cold leg pressure, feedwater fluid temperature, feedwater flow rate, and steam line pressure.

The first calculated solution for the primary side pressure drop likely will be quite close to the desired value. However, the cold leg temperature likely will not match its desired value. This is an indication that the steam generator heat removal rate is not correct. The source of the error is likely to be traced to a poor match between calculated and prototype behavior on the secondary side.

On the secondary side, heat transfer from the tubes to the fluid is controlled by the secondary fluid temperature and the velocity on the outer tube surface. The fluid temperature on the outside of the tubes is affected by the pressure and the recirculation ratio (the ratio of the steam generator downcomer flow rate to the feedwater flow rate). Lower recirculation ratios result in colder fluid entering the tube bundle and better heat removal in the lower region of the tube bundle. Since the majority of the tube length experiences saturated nucleate boiling heat transfer, tube heat transfer is strongly controlled by the secondary fluid saturation temperature. As a result, changes in the secondary side pressure affect the saturation temperature and therefore influence the steam generator heat removal rate. The velocity on the outside of the tubes is also controlled by the recirculation ratio, with higher ratios resulting in higher velocities and therefore higher heat removal rates. RELAP5 provides a one-dimensional (vertically upward) representation of the flow in the steam generator boiler. In the prototype steam generator, however, baffles produce a swirling boiler flow pattern. As a result, the RELAP5-calculated boiler flow velocity is lower than in the prototype and the calculated steam generator heat removal rate is too low.

Achieving a satisfactory simulation of U-tube steam generator secondary steady-state conditions generally requires (a) adjusting flow losses in the steam separator and boiler regions to achieve the desired recirculation ratio, (b) defining a downstream steam line pressure boundary condition (such as at the steam header, cell 800 in Figure 5-5) that provides the desired steam boiler pressure, and (c) using the minimum tube-to-tube spacing as the heated diameter on the secondary side of the tube heat structures to adjust for the multi-dimensional flow patterns of the prototype. Section 5.1.3 provides additional discussion of these adjustments.

#### **5.7.4 Step 3—Coolant Loop with Reactor Coolant Pump**

Figure 5-2 shows the nodalization of the reactor coolant loop. Models for the hot leg, pump suction cold leg, reactor coolant pump, and pump discharge cold leg are merged with the steam generator/steam line model. Step 2 obtained the desired steam generator primary differential pressure and hot and cold leg fluid temperatures when the coolant loop flow rate was prescribed as a boundary condition.

In this step, hot leg fluid temperature, hot leg flow rate, pump discharge cold leg pressure, and reactor coolant pump speed boundary conditions are specified as boundary conditions. In addition, on the secondary side, the boundary conditions from Step 2 are used (feedwater flow rate, temperature, and steam line pressure). The intent of this step is to obtain a satisfactory coolant loop differential pressure with the desired flow rate passing through it. The desired

coolant loop differential pressure is the same as the reactor vessel differential pressure calculated in Step 1.

The wall friction losses in the hot and cold leg pipes are well calculated by RELAP5 and, together with the satisfactory steam generator pressure drop from Step 2, a nearly-satisfactory coolant loop pressure drop is generally obtained on the first attempt. If needed, the loop pressure drop can be modified through minor adjustments in the pump specification (e.g., the pump speed or rated head).

#### 5.7.5 Step 4—Feedwater System

Figure 5-5 shows the nodalization of the feedwater system model. While shown here for completeness, for many applications a detailed model of the feedwater system may not be required. For those applications, it may be sufficient only to specify the feedwater flow rate as a function of time (constant before a turbine trip, then linearly decreasing to zero over a few seconds following a turbine trip). A detailed feedwater system model generally is only required for simulating transients where feedwater flow continues after a turbine trip because of assumed failures.

The feedwater system model is verified by specifying boundary conditions for the condenser temperature, inlet flow rate, heater drain system flow rate and temperature, feedwater heater power, condensate and main feedwater pump speeds, and outlet pressure.

On the inlet side, a TMDPVOL specifies the condenser fluid conditions, typically cold water at a vacuum pressure. A TMDPJUN forces flow from the condenser into the feedtrain at the desired rate. A similar arrangement is used for flow addition from the heater drain system. On the outlet side, the feedwater system model is connected to three TMDPVOLs (one for each steam generator) that specify constant pressure, consistent with the steam generator downcomer pressure obtained from Step 2.

Model tune-up should start at the steam generators and proceed upstream toward the condenser. Adjustments to the flow losses are made as needed to obtain the desired pressures within the system (typically, these are known at several locations). The losses are most uncertain across valves and heat exchangers, so adjustments at these locations often can be justified. Adjustments to pump parameters also may prove beneficial (see the discussion in Step 3).

The feedwater system model tune-up process can be considered successful when a satisfactory agreement is obtained between the calculated condensate pump inlet pressure and the desired condenser pressure (which was used as the inlet boundary condition). To allow this comparison to be made, it will be necessary to add a hydrodynamic calculational cell (e.g., a single-volume or branch component) between the condensate pump and condenser (components 824 and 822 in Figure 5-5). When agreement has been obtained, the additional cell is removed and the TMDPJUN is replaced with a normal junction (in this example the inlet junction of pump 824).

### 5.7.6 Step 5—Formation of the System Model

Steps 1 through 4 have produced models of the reactor vessel, steam generator/steam line, coolant loop, and feedwater systems that satisfactorily simulate the individual performance of these systems during full-power plant operation. Furthermore, the calculated conditions for these individual models are consistent at their adjoining boundaries.

Before combining the individual models into a system model, it is best to substitute the calculated steady conditions as the input initial conditions for each of the individual models. Recall that crude approximations of the initial conditions were input when the model was first assembled. Steps 1 through 4 have calculated the actual initial conditions (pressures, temperatures, flow rates, etc.) that represent full-power steady operation. If done by hand, this substitution is quite tedious; automated techniques for this process are available. It is not essential to substitute the initial conditions because the system model (including the modifications made from Steps 1 through 4) can be executed successfully to the desired steady solution. However, substituting the steady conditions into the input listing at this time is advantageous because it minimizes the computer time needed to obtain a steady-state solution with the system model.

Two copies of the coolant loop model from Step 3 are made to simulate the other coolant loops in the plant. The component numbers on the copies are then changed, since each component must have a unique number. It is convenient if the same components in each of the loops have similar numbers. One method is to increment the hundreds digit from loop to loop (e.g., let components 206, 306, and 406 represent a comparable feature in the three loops).

The reactor vessel model from Step 1 is combined with the three coolant loop models, and the feedwater system model from Step 4 is appended to the steam generators on the coolant loops. The pressurizer model (see Figure 5-4) is then appended at the hot leg/surge line and cold leg/spray line connection points. When combining models, care must be taken to remove the components that were used to provide boundary conditions in previous steps, and to add hydrodynamic junctions to appropriately join the individual models. Referring to Figure 5-5, at this time it will be necessary to connect the three individual steam lines to the common header and add the common steam line (components 800, 802, 804, 806, 808, and 810) to the model. The modeler is required to specify the turbine header pressure (component 806) such that the steam header pressure (component 800) is the same as was used in Steps 2 and 3. The steam pressure boundary condition effectively is moved downstream to the turbine header. In practice, it is usually adequate to estimate the turbine header pressure by hand-calculating the pressure drop down the steam line and through the turbine stop valve.

The combined system model may now be executed as a unit. The boundary conditions remaining from the individual models are condenser pressure and fluid temperature; feedwater heater drain flow rate and fluid temperature; turbine header steam pressure; speeds for the main coolant, main feedwater, and condensate pumps; and powers for the core and feedwater heaters. In addition, it is necessary to add a boundary condition for the primary coolant system pressure. In the prototype, this function is provided by the pressurizer heaters and spray control systems that are not yet activated in the model. It is convenient to provide this pressure boundary condition by temporarily connecting a TMDPVOL (with the desired pressure specified) through a

single junction at a location in the primary coolant system where the pressure is well known. For example, this function might be accomplished by connecting a TMDPVOL (with the hot leg pressure and hot leg fluid temperature) to one of the hot leg components. This temporary TMDPVOL will donate liquid to, or accept liquid from, the reactor coolant system as needed to maintain the desired hot leg pressure.

If the previous steps have been accomplished successfully, the conditions calculated with the combined model should differ only slightly from the desired conditions calculated with the individual models. At this stage, adjustments in the primary side flow rates may be accomplished with minor changes in the reactor coolant pump speed. Once the desired flow rate is attained, the hot-to-cold leg differential temperature will be correct; however, the average coolant temperature (i.e., the average of the hot and cold leg temperatures) may be slightly high or low. This condition may be remedied by minor adjustment of the secondary system pressure (specified as a boundary condition at the turbine header).

At this point, the combined model will be executed through a null transient for a period of time to allow steady conditions to be achieved. Generally, this process requires a few hundred seconds of transient time to accomplish.

#### 5.7.7 Step 6—Control Systems

The control systems that are active during normal plant operation are added to the model at this point. These systems include the steam generator level control, pressurizer pressure control, and pressurizer level control functions described in Section 5.1.7. Implementation of the control systems into the model has been delayed until this point because they require various calculated plant parameters as input. These parameters have not been available until Step 5 was completed. The input for the control systems is carefully reviewed and, if necessary, the controller initial conditions, biases, and set points are modified based on the calculated steady-state plant parameters. The temporary primary system pressure boundary condition imposed in Step 5 is then removed from the model.

The system model is executed again through a null transient, this time with the RELAP5 control system models activated. This step is successfully completed when the controllers have driven their dependent variables (steam generator level, pressurizer level, and pressurizer pressure) to the desired values. A few hundred seconds of transient time are typically required to accomplish this process.

#### 5.7.8 Step 7—Models of Non-operating Systems

Models of plant features, systems, trips, and control systems that are not activated during normal plant operation are now added to the model. These features include

- Accumulators
- High- and low-pressure injection systems
- Pressurizer power-operated relief valve and code safety valves
- Main steam isolation valves
- Steam generator power-operated relief valves and safety valves

- Auxiliary feedwater systems
- Turbine stop valve
- Steam dump valves.

Since performance of these systems cannot be checked at the full power initial condition, it is important that the modeler independently check their performance.

Some of these independent checks can be made using simple models. For example, the RELAP5-calculated flow through a PORV can be independently checked against the valve design data using a model employing a valve and a few hydrodynamic cells. However, other checks will have to wait until the model development is complete, a successful steady-state condition has been calculated, and an active transient simulation is performed (see Step 8). For example, it is necessary to perform an active transient calculation to determine if a PORV model opens and closes as intended.

A short null transient is run with the inactive features included in the model. This transient will confirm that input errors do not exist and that the inactive features do not, in fact, affect the steady-state solution.

#### **5.7.9 Step 8—Final Tune-Up and Check-Out**

A final check of the calculated full-power steady conditions is made. The modeler should check many, not just a few, plant parameters for steadiness. Generally, a completely stable set of conditions is not attained; some minor drifting of parameters continues. The modeler should determine the source of the drift and consider if its magnitude is acceptable. Common sources of drift are thermal gradients within the thicker heat structures of the model. For example, consider the reactor vessel wall with gamma heating. The wall is about five inches thick and the thermal time constant is such that perhaps thousands of null transient seconds are required for its thermal gradient to stabilize. In this case, the thermal capacity of the material may be artificially lowered, allowing the heat structure gradient to be quickly established during a null transient calculation. Once the proper gradient has been calculated, the true thermal capacity is restored to the model.

An active transient calculation should be performed to check the performance of plant features, trips, systems, and controllers that are not active during full power operation. Adjustments and corrections are implemented as appropriate.

At this point, the model is considered complete and confirmed. It is recommended that the final steady conditions attained be substituted back into the final model that created them (see discussion in Step 5). In this manner, the final form of the model is a complete input stream that includes the true steady initial conditions. From a quality assurance viewpoint, this method is advantageous because a single master file documents the complete model and its initial state. When it is desired to perform an active transient calculation, the master file is copied, and the model changes implementing the transient are incorporated into the copy. This new file may then document the complete model, the initial conditions, and the changes made.



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APPENDIX A

ABSTRACTS OF RELAP5/MOD3 REFERENCE DOCUMENTS

## APPENDIX A

### ABSTRACTS OF RELAP5/MOD3 REFERENCE DOCUMENTS

Adams, J. P., C. A. Dobbe, and P. D. Bayless, 1986, "Numerical Simulation of PWR Response to a Small Break LOCA with Reactor Coolant Pumps Operating," *4th International Symposium on Multi-Phase Transport and Particulate Phenomena, Miami Beach, Florida, December 1986*, EGG-M-32686.

Calculations have been made of the response of pressurized water reactors (PWRs) during a small break loss-of-coolant accident with the reactor coolant pumps (RCPs) operating. This study was conducted, as part of a comprehensive project, to assess the relationship between measurable RCP parameters, such as motor power or current, and fluid density, both local (at the RCP inlet) and global (average reactor coolant system). Additionally, the efficiency of using these RCP parameters, together with fluid temperature, to identify an off-nominal transient as either a loss-of-coolant accident, a heatup transient, or a cooldown transient and to follow recovery from the transient was assessed. The RELAP4 and RELAP5 computer codes were used with three independent sets of RCP two-phase degradation multipliers. These multipliers were based on data obtained in two-phase flow conditions for the Semiscale, LOFT, and Creare/Combustion Engineering Electric Power Research Institute pumps, respectively. Two reference PWRs were used in this study: Zion, a four-loop, 1100-MWe Westinghouse plant operated by Commonwealth Edison Co. in Zion, Illinois and Bellefonte, a two-by-four loop, 1213 MWe Babcock and Wilcox designed plant being built by the Tennessee Valley Authority in Scottsboro, Alabama. The results from this study showed that RCP operation resulted in an approximately homogeneous reactor coolant system and that this result was independent of the reference plant, computer code, or two-phase RCP head degradation multiplier used in the calculation.

Aksan, S. N., G. T. Analytis, and D. Luebbesmeyer, 1989, "Switzerland's Code in Support of the International Code Assessment Program (ICAP)," *16th Water Reactor Safety Information Meeting, March 1989, Gaithersburg, Maryland*, Paul Scherrer Institute, Wuerealingen, Switzerland.

Within the framework of the International Code Assessment Program (ICAP) of the U.S. Nuclear Regulatory Commission, independent code assessment analyses at the Paul Scherrer Institute have been performed using the RELAP5/MOD2 and TRAC-BD1/MOD1 thermal hydraulic transient codes. The assessment cases selected include both separate effects and integral tests. The calculations and analysis of most of the agreed assessment cases have been completed in this paper, and the main results and conclusions of these calculations are presented. As a result of these calculations and analysis, model changes are proposed for a number of special models that need to be further improved. Some of these proposals were tested in an experimental version of RELAP5/MOD2 at the Paul



Scherrer Institute. The rapid cladding cooling and quench during the blowdown phase of a large break loss-of-coolant has also been investigated in some detail. The experimental evidence available from blowdown quench, such as that encountered in the loss-of-fluid test (LOFT) experiments, is reviewed. Calculations using the RELAP5/MOD2 code have been performed for the Organization for Economic Cooperation and Development/LOFT LP-LB-1 and LP-02-6 tests to identify the codes ability to calculate the blowdown phase quench. To further investigate rapid cladding quenches, separate effects tests conducted in the LOFT Test Support Facility have been calculated using a frozen version of RFLAP5/MOD2. The preliminary results of these calculations and the conclusion are also presented.

Analytis, G. T., 1987, "Implementation and Assessment of Drift-Flux Post-Dryout Interfacial Shear Model in RELAP5/MOD2/36.02," *Transactions of the American Nuclear Society*, 55, pp. 707-709.

Interfacial shear  $f_{/sub i/}$  and heat transfer to the liquid  $h_{/sub il/}$  are of paramount importance for the correct prediction of liquid carryover and rod surface temperatures during reflooding. It has been shown recently that a new drift-flux model based bubble/slug  $f_{/sub i/}$  correlation for rod bundles greatly improves the predicting capabilities of the RELAP5/MOD2/36.02 model in the analysis of boil-off and low flooding rate experiments.

Analytis, G. T., and M. Richner, 1986, "Effect of Bubbly/Slug Interfacial Shear on Liquid Carryover Predicted by RELAP5/MOD2 During Reflooding," *American Nuclear Society and Atomic Industrial Forum Joint Meeting, Washington, D. C., November 1986*, Wuorenlingen, Switzerland.

Analysis of very low flooding rate reflooding experiments and one boiloff experiment in the 33 electrically heated rod bundle NEPTUN<sup>1</sup> at the Swiss Federal Institute for Reactor Research with RELAP5/MOD2/36.02 has shown that the code grossly overpredicts the liquid carryover. Similar results have been reported in the analysis of a large number of boiloff experiments in NEPTUN with TRAC-BD1/MOD1. In this case, the differences between measurements and predictions were attributed to the large bubble/slug interfacial shear in TRAC-BD1, and excellent agreement with the measurements was achieved by implementing a slightly modified version of a new bubbly/slug interfacial shear correlation developed for rod bundles. As far as reflooding is concerned, one of the most crucial parameters for the correct prediction of the rod surface temperature histories is the interfacial shear  $f_{/sub i/}$  in the different flow regimes; this term will largely determine the liquid fraction at certain axial elevation and the liquid carryover. The authors outline the implementation of the new bubble/slug  $f_{/sub i/}$  correlation in RELAP5/MOD2/36.02 and assess its influence in the liquid carryover in the analysis of low flooding rate experiments in NEPTUN.

Analytis, G. T., and M. Richner, 1986, *Implementation and Assessment of a New Bubbly/Slug Flow Interfacial Friction Correlation in RELAP5/MOD2/36.02*, TM-32-86-10, January, Swiss Federal Institute for Reactor Research, Wuorenlingen, Switzerland.

Analysis of boil-off and low flooding rate reflooding experiments in the rod bundle NEPTUN with RELAP5/MOD2 has shown that the code grossly underpredicts the collapsed liquid level history in the test section because it over-predicts the amount of water expelled. Similar problems were encountered in the analysis of the same boil-off experiments with TRAC-BD1 Version 12 and MOD1 and were resolved by implementing a new bubbly/slug flow interfacial friction correlation in this code. The authors report on the implementation of the new interfacial friction correlation in RELAP5/MOD2/36.02 as well as its consequences on the predicted collapsed liquid level histories in the rod bundle NEPTUN.

NOTE: This report is restricted to International Code Assessment Program members, unless specific permission is granted by the author.

Analytis, G. T., M. Richner, and S. N. Aksan, 1987, *Assessment of Interfacial Shear and Wall Heat Transfer of RELAP5/MOD2/36.02 During Reflooding*, EIR-Bericht Nr. 624, May 1, Eidgenoessisches Inst. fuer Reaktorforschung, Wuerenlingen Switzerland.

The analysis of a number of reflooding and one boil-off experiment in the electrically heated rod bundle NEPTUN at the Swiss Federal Institute for Reactor Research with RELAP5/MOD2/36.02 showed significant differences between measurements and predictions. The same was true for the analysis of two FLECHT-SEASET reflooding experiments. The authors report on these items and present the modifications made to the frozen version of RELAP5/MOD2/36.02. These changes eliminate most of the observed discrepancies.

Analytis, G. T., M. Richner, and S.N. Aksan, 1987, "Qualification of Modifications of Interfacial Shear and Wall Heat Transfer of RELAP5/MOD2/36.02 During Reflooding," *Transactions of the American Nuclear Society*, 55, pp. 705-707.

Extensive assessment of RELAP5/MOD2/36.02 has been performed by using reflooding experiments performed at the heater rod bundle NEPTUN at the Swiss Federal Institute for Reactor Research and at the FLECHT-SEASET test facility. As a result of this work, a number of modifications were made in the interfacial shear and reflooding wall heat transfer packages of the code. The modifications are represented in this work.

Analytis, G. T., M. Richner, M. Andreani, and S. N. Aksan, 1987, "Assessment of Uncertainty Identification for RELAP5/MOD2 and TRAC-BD1/MOD1 Codes Under Core Uncovery and Reflooding Conditions," *14th Water Reactor Safety Information Meeting, Gaithersburg, Maryland, October 27, 1986*, NUREG/CP-0082, Volume 5, pp. 329-370, February, Swiss Federal Institute for Reactor Research, Wuerenlingen, Switzerland.

Assessment calculations for the thermal hydraulic transient computer codes RELAP5/MOD2 (frozen version 36.02) and TRAC-BD1/MOD1 (frozen version 22) were performed, at the Swiss Federal Institute for Reactor Research (EIR) under both core uncovery (boil-off) and reflooding conditions. The aim of the work was to assess the predicting capabilities of the frozen versions of the best estimate computer codes. Some of the reflooding and boil-off experimental data observed from the NEPTUN test facility at

FIR were used for the assessment work. Model optimization calculations on nodalization and the effect of available options (e.g., heat slab sizes) are performed with a selected base case, and the same model is applied to the other experimental cases, covering a wide range of parameters. The authors report the results of these assessment calculations and identify and point out the existing uncertainty areas in boil-off and reflooding phenomena.

Ardron, K. H., and W. M. Bryce, 1988, "Assessment of RELAP5/MOD2 by Comparison with Separate Effects Experiments," *Third International Topical Meeting on Nuclear Power Plant Thermal Hydraulics and Operations, November 1988, Seoul, Korea.*

Two studies are described in which models in the RELAP5/MOD2 code are assessed by comparison with separate effects tests. In the first study, the horizontal stratification model in RELAP5/MOD2 is assessed. This model describes the flow of two-phase mixture through a small diameter off-take connected to a horizontal pipe containing a stratified flow. Comparison with separate effects test data show that the model systematically underpredicts the quality in the off-take branch. A modified code version containing improved correlations gives improved agreement with the separate effects tests and with an integral test in the Loss-of-Fluid Test Facility.

In the second study, RELAP5/MOD2's ability to describe the counter current flooding limit (CCFL) is assessed using a test problem to show that the CCFL is calculated in a pressurized water reactor steam generator tube. A large overprediction of the CCFL limit is attributed to the special treatment in RELAP5/MOD2 for calculating interphase friction under conditions where void fraction decreases with elevation.

Ardron, K. H., and A. J. Ciate, 1989, *Assessment of Interphase Drag Correlations in the RELAP5/MOD2 and TRAC-PF1/MOD2 Codes*, July, Central Electricity Generating Board, Barnwood UK.

An assessment is carried out of the interphase drag correlations used in modeling vertical two-phase flows in the advanced thermal hydraulic codes RELAP5/MOD2 and TRAC-PF1/MOD1. The assessment is performed by using code models to calculate void fraction in fully developed steam-water flows, and comparing results with predictions of standard correlations and test data. The study is restricted to the bubbly and slug flow regimes (void fractions below 0.75). For upflows, at pressures of interest in pressurized water reactor small break loss-of-coolant accident and transient analysis, the performance of the code models is generally satisfactory. Exceptions are (a) small hydraulic diameter channels at low pressures ( $p$  equal to or less than 4 MPa) (b) large pipe diameters at void fractions exceeding 0.5. In these cases, void fraction errors are outside normal uncertainty ranges. For downflows, the code models give good agreement with limited available void fraction data. The numerical results given in this paper allow a rapid estimate to be made of void fraction errors likely to arise in a particular code application from deficiencies in interphase drag modeling.

Ardron, K. H., and P. C. Hall, 1988, "UK Experience with RELAP5/MOD2," *15th Water Reactor Safety Information Meeting, Gaithersburg, Maryland, October 26, 1987*, February, Central Electricity Generating Board, Gloucester England.

RELAP5/MOD2 is being used in the United Kingdom (UK) for analysis of small loss-of-coolant accidents and pressurized transients in a Sizewell B pressurized water reactor. To support this application and gain familiarity with the code, the Central Electricity Generating Board the United Kingdom Atomic Energy Authority (UKAEA) have analyzed a number of integral and separate effects tests with RELAP5/MOD2. Several reports on this work have been sent to the U.S. Nuclear Regulatory Commission (NRC) under a UK/NRC bilateral agreement. This paper presents a review of UK experience with RELAP5/MOD2 since the code was received in the UK in February 1985. Calculations are described of small loss-of-coolant accidents and pressurized transient experiments in the LOFT and LOBI test facilities, and boil-down tests in the UKAEA THETIS facility. Code calculations are also compared with data on pull-through/entrainment effects in two-phase flow in an off-take branch connected to a horizontal pipe containing stratified flow. The code has generally performed well in the calculations attempted so far, and appears to represent a considerable improvement over earlier versions of RELAP5 in respect of stability, running speed, mass conservation errors, and accuracy. The modeling difficulties identified in the UK studies have been defects in the horizontal stratification entrainment model, used to calculate discharge from a side branch connected to a horizontal pipe in which there is stratified flow, and deficiencies in critical flow calculations when there is separated flow in the volume upstream of the break. Some calculations are described with modified code versions containing improved models to illustrate the deficiencies.

Babcock & Wilcox Owners Group Analysis Committee, 1986, *RELAP5/MOD2 Benchmark of OTIS Feed and Bleed Test #220899*, BAW-1903, March.

The Once-Through Integral System (OTIS) facility was designed and built for the investigation of thermal hydraulic phenomena associated with small break loss-of-coolant accidents. The facility is a one-loop (one hot leg, one steam generator, and one cold leg) scaled representation of a Babcock & Wilcox (B&W) 205 fuel assembly raised loop plant. In March 1984, OTIS Test 220899 was completed. Important phenomena observed include primary liquid cooldown, primary system depressurization with the pressurizer filling and the pressurizer solid, and impact of reactor vessel vent valves on core cooling and loop flows. The objective of this analysis is to simulate OTIS Test 220899 with the current B&W version of RELAP5/MOD2 (Cycle 36). The hot leg U-bend and steam generator nodding are consistent with the modeling used for the Multiloop Integral System Test facility. A detailed system description of the OTIS facility in parallel with a discussion of the RELAP5 model is presented. Results of the study and concluding comments are also presented.

Bayless, P. D., and R. Chambers, 1984, *Analysis of a Station Blackout Transient at the Seabrook Nuclear Power Plant*, EGG-NTP-6760, September.

A postulated station blackout transient at the Seabrook Nuclear Power Plant was analyzed in support of the U.S. Nuclear Regulatory Commission's Severe Accident Sequence Analysis Program. The RELAP5/MOD2 and SCDAP/MOD1 computer codes were used to



calculate the transient from initiation through severe core damage. The base transient, the "TMLB" sequence, assumed no offsite power, onsite power, emergency feedwater, or operator actions. Additional analyses investigated the sensitivity to the core modeling and a potential mitigating action.

Bayless, P. D., C. A. Dobbe, and R. Chambers, 1987, *Feedwater Transient and Small Break Loss of Coolant Accident Analyses for the Bellefonte Nuclear Plant*, NUREC/CR-4741, EGG-2471, March.

Specific sequences that may lead to core damage were analyzed for the Bellefonte Nuclear Plant as part of the U. S. Nuclear Regulatory Commission's Severe Accident Sequence Analysis Program. The RELAP5, SCDAP, and SCDAP/RELAP5 computer codes were used in the analyses. The two main initiating events investigated were a loss of all feedwater to the steam generators and a small cold leg break loss-of-coolant accident. The transients of primary interest within these categories were the TMLB' and S2D sequences. Variations on systems availability were also investigated. Possible operator actions that could prevent or delay core damage were identified, and two were investigated for a small break transient. All of the transients were analyzed until either core damage began or long-term decay heat removal was established. The analyses showed that for the sequences considered, the injection flow from one high-pressure injection pump was necessary and sufficient to prevent core damage in the absence of operator actions. Operator actions were able to prevent core damage in the S2D sequence, no operator actions were available to prevent core damage in the TMLB' sequence.

Beelman, R. J., W. H. Grush, G. A. Mortensen, D. M. Snider, and K. L. Wagner, 1989, "RELAP5 Desktop Analyzer," *International RELAP5 Users Seminar, College Station, Texas, January 31, 1989*

The previously mainframe-bound RELAP5 reactor safety computer code has been installed on a microcomputer. A simple color-graphic display driver has been developed to enable the user to view the code results as the calculation advances. To facilitate future interactive desktop applications, the Nuclear Plant Analyzer (NPA), also previously mainframe-bound, is being redesigned to encompass workstation applications. The marriage of RELAP5 simulation capabilities with NPA interactive graphics on a desktop workstation promises to revolutionize reactor safety analysis methodology.

Blanchat, T., and Y. Hassan, 1989, "Comparisons of Critical Heat Flux Correlations with Bundle Flows," *Annual Meeting of the American Nuclear Society, Atlanta, Georgia, June 1989.*

The critical heat flux has been the subject of research in the field of boiling heat transfer by nuclear engineers for many decades. The objective of this study is to predict the behavior of the secondary side of the once-through steam generator using the RELAP5/MOD2 computer code and, in particular, to obtain a better prediction of critical heat flux in bundles

Blanchat, T. K., and Y. A. Hassan, 1988, "Thermal-Hydraulic Analysis of a Nuclear Once Through Steam Generator Using RELAP5/MOD2 Computer Code," *Third International Topical*



*Meeting on Nuclear Power Plant Thermal Hydraulics and Operations, Seoul, Korea, November 1988.*

A RELAP computer code model for a once-through steam generator has been developed. Parametric studies were conducted. Underprediction of the heat transfer in the nucleate boiling flow was mitigated (or corrected) by reducing the hydraulic diameter through the use of the small distance between the tubes. A new flow regime map for flow in bundles was developed and implemented in the code. This new flow regime map more accurately predicts transition for slug-to-annular flow. Consequently, improved saturated conditions for the fluid flow at the entrance to the boiler were obtained.

Blanchat, T. K., and Y. A. Hassan, 1987, "Comparison Study of the Westinghouse Model E Steam Generator Using RELAP5/MOD2 and RETRAN-02," *Transactions of the American Nuclear Society*, 55, pp. 699-701.

The response of a steam generator during both operational and transient conditions is of major importance in studying the thermal hydraulic behavior of a nuclear reactor coolant system. The objective of this study is to predict the behavior of the secondary side of the Westinghouse Model E steam generator using the RELAP5/MOD2 computer code. Steady-state conditions and a loss-of-feedwater transient were predicted and compared with a previous study using the RETRAN-02 computer code. The comparison showed an agreement with the previous study for steady-state calculations.

Bolander, M. A., 1989, *RELAP5/MOD2.5 Thermal Hydraulic Analysis for an Alternate Fuel Design in the N Reactor*, EGG-EAST-8362, June.

This report documents work performed at the Idaho National Engineering Laboratory in support of the Westinghouse Hanford Company safety analyses of the N Reactor. This work included (a) developing a RELAP5/MOD2.5 N Reactor separate effects alternate fuel design model, (b) performing a RELAP5/MOD2.5 computer code validation for N Reactor applications, (c) performing a radiation heat transfer sensitivity study to observe the effects of radiation heat transfer for a design-basis accident, and (d) performing and analyzing RELAP5/MOD2.5 scoping calculations using the alternate fuel design model for a design basis accident.

Bolander, M. A., 1988, *Simulation of a Cold Leg Manifold Break Sequence in the N Reactor with a Failure of an ECCS CV-2R Valve*, EGG-TFM-7988, February.

This final report documents our analyses of the cold leg manifold break with one ECCS CV-24 check valve failing to open.

Bolander, M. A., and C. D. Fletcher, 1988, *Simulation of Cold Leg Manifold Break and Station Blackout Sequences in the N Reactor*, EGG-TFM-7891, February.

This report documents work performed at the Idaho National Engineering Laboratory in support of the Westinghouse Hanford Company safety analyses of the N Reactor. This work included (a) developing a RELAP5/MOD2 N Reactor model from information

contained in an existing RETRAN model, (b) modifying the RELAP5/MOD2 computer code for simulation of reflood behavior in horizontal core channels, and (c) performing and analyzing RELAP5/MOD2 transient calculations simulating N Reactor response during two hypothetical accidents.

Bolander, M. A., and C. D. Fletcher, 1988, *Simulation of Inlet and Outlet Riser Break Sequences in the N Reactor*, EGG-TFM-7930, February.

This report documents work performed at the Idaho National Engineering Laboratory in support of the Westinghouse Hanford Company safety analyses of the N Reactor. The RELAP5/MOD2 computer code was used in analyzing two hypothetical transients. The computer code was modified specifically to simulate the refill behavior in the N Reactor process tubes. The transients analyzed were a double-ended rupture of an inlet riser column and a double-ended rupture of an outlet riser column.

Bolander, M. A., J. C. Chapman, and C. D. Fletcher, 1988, *Simulation of Cold Leg Manifold Break and Station Blackout Revised Sequences for Reduced ECCS (Emergency Core Cooling System) in the N Reactor*, EGG-TFM-7962, February.

This report presents analyses of two loss-of-coolant accident sequences of the N Reactor using the RELAP5/MOD2 computer code. RELAP5/MOD2 is a best-estimate, two-phase, nonhomogeneous, nonequilibrium, thermal hydraulic, computer code designed for light water pressurized reactor transients. The N Reactor is a graphite-moderated, pressurized water reactor. The primary coolant is channeled through 1003 horizontal pressure tubes that contain two concentric tubular metallic fuel elements. The two accident sequences simulated were a double-ended guillotine break in the cold leg manifold and a station blackout. Both simulations cover the period beginning with the (a) initiating event, (b) either the break or the loss of ac power, and (c) the stabilization of the core fuel element temperatures. (The station blackout calculation was carried out until the core was quenched.) The discussion presented in this report includes brief descriptions of the N Reactor, the computer code and specific code modifications for horizontal reflood, and the computer code model used for the simulation. The results and the analyses of the two calculations are also presented.

Bolander, M. A., C. D. Fletcher, C. B. Davis, C. M. Kullberg, B. D. Stitt, M. E. Waterman, and J. D. Burt, 1984, "RELAP5 Thermal-Hydraulic Analyses of Overcooling Sequences in a Pressurized Water Reactor," *International Meeting on Thermal Nuclear Reactor Safety, Karlsruhe, Federal Republic Germany, September 1984*, KFK-3880/1, pp. 311-319.

In support of the Pressurized Thermal Shock Integration Study, the Idaho National Engineering Laboratory has performed analyses of overcooling transients using the RELAP5/MOD1.6 and MOD2 computer codes. These analyses were performed for the H. B. Robinson Unit 2 pressurized water reactor, a Westinghouse 3-loop design plant. Results of the RELAP5 computer codes as a tool for analyzing integral plant transients requiring a detailed plant model, including complex trip logic and major control systems, are examined.

Boone, J., 1989, *KFACT Form Loss Coefficient: Calculations for RELAP5/MOD2 Input Decks*, Duke Power Company, September.

This document and the source code are Duke Power proprietary and cannot be distributed without prior consent of Duke Power.

Boucher, T. J., 1985, *Quick Look Report for Semiscale MOD-2C Test S-FS-2*, EGG-SEMI-6827, March.

**ABSTRACT:** Results of a preliminary analysis of the first test performed in the Semiscale MOD-2C Steam Generator Feedwater and Steam Line Break (FS) experiment series are presented. Test S-FS-2 simulated a pressurized water reactor transient initiated by a double-ended offset shear of a steam generator main steam line upstream of the flow restrictor. Initial conditions represented normal "hot-standby" operation. The transient included an initial 600-s period in which only automatic plant protection systems responded to the initiating event. This period was followed by a series of operator actions necessary to stabilize the plant at conditions required to allow a natural circulation cooldown. The test results provided a measured evaluation of the effectiveness of the automatic responses in minimizing primary system overcooling and operator actions in stabilizing the plant. Test data were compared with the RELAP5/MOD2 computer code and also provided a basis for comparison with other tests in the series of the effects of break size on primary overcooling and primary-to-secondary heat transfer.

Boucher, T. J., and D. G. Hall, 1985, *Quick Look Report for Semiscale MOD-2C Test S-FS-6*, EGG-SEMI-7022, September.

Results of a preliminary analysis of the third test performed in the Semiscale MOD-2C Steam Generator Feedwater and Steam Line Break (FS) experiment series are presented. Test S-FS-6 simulated a pressurized water reactor transient initiated by a 100% break in a steam generator bottom feedwater line downstream of the check valve. With the exception of primary pressure, the initial conditions represented the initial conditions used for the CE System 80 Final Safety Analysis Report (FSAR) Appendix 15B calculations. The transient included an initial 600-s period in which only automatic plant protection systems responded to the initiating event. This period was followed by a series of operator actions necessary to stabilize the plant and a subsequent operator controlled natural circulation cooldown and depressurization with upper heat void collapse method investigations. The test results provided a measured evaluation of the effectiveness of the automatic responses in minimizing primary system overpressurization and operator actions in stabilizing and recovering the plant. Test data were compared with the RELAP5/MOD2 computer code and also provided a basis for comparison with other tests in the series of the effects of break size on primary overpressurization and primary-to-secondary heat transfer.

Brain, C. R., 1990, "Post-test Analysis of Natural Circulation, Flow Coastdown, and Pressurizer Spray Tests in a Large Four Loop PWR Using RELAP5/MOD2," *Technical Committee/Workshop on Computer Aided Safety Analysis, Berlin German Democratic Republic, Computer Aided Safety Analysis 1989, April 1990*, IAEA-TC-560.03, Central Electricity Generating Board, Barnwood, Gloucester United Kingdom.

This paper describes a series of calculations performed by the Central Electricity Generating Board to assess the RELAP5/MOD2 input dataset for the Sizewell B nuclear power plant. Given the similarities of Sizewell B with the Westinghouse Standardized Nuclear Unit Power Plant System plants, results of commissioning tests from Callaway nuclear power plant and Wolf Creek were used in the validation process. Results presented demonstrate a good agreement between test data and calculations.

Brittain, I., 1985, "UK Experience with TRAC-PF1/MOD1 and RELAP5/MOD2," *13th Water Reactor Safety Information Meeting, Washington, D.C.*, October 1985, United Kingdom Atomic Energy Authority.

The United Kingdom has been using versions of TRAC and RELAP5 for best-estimate pressurized water reactor loss-of-coolant accident analysis for a number of years. In the preconstruction phase of the Sizewell B plant, the codes were used to provide an independent assessment that could be compared with the evaluation model-based safety case. It is generally agreed that advanced code calculations will play a more direct role in the pre-operation phase of the project, though the precise use has not yet been determined. The author's experience with RELAP5/MOD2 is limited, and consists of collaboration in some of the code development preliminary work in analyzing Loss-of-Fluid Test small break tests, and carrying out small break sensitivity studies for the Sizewell B plant.

Brittain, I., and S. N. Aksan, 1990, *OECD-LOFT Large Break LOCA Experiments: Phenomenology and Computer Code Analyses*, PSI-Bericht Nr.72 AEEW-TRS-1003, August, (United Kingdom Atomic Energy Authority Atomic Energy Establishment, Winfrith, United Kingdom); S.N. Paul Scherrer Institute, Viligen, Switzerland.

Large break loss-of-coolant accident data from the Loss-of-Fluid Test (LOFT) are a very important part of the world database. This paper describes the two double-ended cold leg break tests LP-02-6 and LP-LB-1 carried out within the Organization for Economic Cooperation and Development (OECD) LOFT Program. Tests in LOFT were the first to show the importance of both bottom-up and top-down quenching during blowdown in removing stored energy from the fuel. These phenomena are discussed in detail, together with the related topics of the thermal performance of nuclear fuel and its simulation by electric fuel rod simulators, and the accuracy of cladding external thermo-couples. The LOFT data are particularly important in the validation of integral thermal hydraulic codes such as TRAC and RELAP5. Several OECD partner countries contributed analyses of the large break tests. Results of these analyses are summarized and some conclusions are given.

Burt, J. D., C. A. Dobbe, and P. D. Wheatley, 1988 *Advanced Test Reactor Large Break Loss-of-Coolant Accident Break Spectrum Study*, EGG-TFM-8082, April.

This report documents work performed at the Idaho National Engineering Laboratory in support of the U.S. Department of Energy's safety review of the Advanced Test Reactor. Four large break loss-of-coolant transients were calculated using the RELAP5/MOD2

computer code to determine the worst transient in terms of vessel inventory loss and core cladding temperatures.

Callow, R. A., 1988, *Thermal-Hydraulic Response and Iodine Transport During a Steam Generator Tube Rupture*, EGG-EAST-8264, October.

Recent reanalyses of the offsite dose consequences following a steam generator tube rupture have identified a possible non-conservative in the original Final Safety Analysis Report analyses. Post-trip uncovering of the top of the steam generator U-tubes, in conjunction with a break near the U-tube top, could lead to increased iodine release because of a reduced "scrubbing" of the iodine in the primary break fluid by the steam generator secondary liquid. To evaluate this issue, analyses were performed at the Idaho National Engineering Laboratory. The RELAP5 computer code was used to conduct an analysis of the Surry plant to determine whether the post-trip steam generator secondary mixture level was sufficient to maintain continuous coverage of the U-tubes. The RELAP5 result was supported by a hand calculation. Additional RELAP5 analyses were conducted to determine the magnitude of iodine release for a steam generator tube rupture. Two sensitivity studies were conducted. The amount of iodine released to the atmosphere was strongly dependent on the assumed value of the partition coefficient. The assumption of steam generator U-tube uncovering on a collapsed liquid level basis following reactor trip had a minor effect on the amount of released iodine.

Caraher, D., 1987, *RELAP5 Simulations of a Hypothetical LOCA in Ringhals 2*, STUDEVIK-NP-87-105, September 18, Swedish Nuclear Power Inspectorate, Stockholm; Studsvik Energiteknik AB, Nykoeping, Sweden.

RELAP5 simulations of a hypothetical loss-of-coolant accident in Ringhals 2 were conducted to determine the sensitivity of the calculated peak cladding temperature (PCT) to Appendix K requirements. The PCT was most sensitive to the assumed model decay heat: changing from the 1979 American Nuclear Society standard to 1.2 times the 1973 standard increased the cladding temperature by 70 to 100 K. After decay heat, the two parameters that most affected the PCT were steam generator heat transfer and heat transfer lockout. The PCT was not sensitive to the assumed pump rotor condition (locked vs. coasting), nor was it sensitive to a modest amount (5 - 10%) of steam generator tube plugging.

Caraher, D., and R. Shumway, 1989, *Enhanced RELAP5/MOD3 Surface-to-Surface Radiation Model*, EGG-EAST-8442, February.

The RELAP5/MOD2 computer program lacked the ability to do surface-to-surface radiation heat transfer. A model was developed by Intermountain Technologies Incorporated that allowed any of the regular RELAP5 heat slabs to radiate to any other heat slab. However, the model only allowed for one set of communicating heat slabs. The model has been enhanced to allow for up to 99 sets of communicating heat slabs. In addition, the slabs can now be modified upon restart. The view factors and surface insolvents must be specified by the user. Absorbing fluid between the two surfaces is not considered except that the user can choose the void fraction below which the radiation



model is inactive. To verify that the model was properly accounting for radiant energy transfer, the Gota radiation test was repeated with excellent results. The updates have been exercised on the Cray at the Idaho National Engineering Laboratory.

Caraher, D. L., and R. W. Shumway, 1989, *Metal-Water Reaction and Cladding Deformation Models for RELAP5/MOD3*, EGG-EAST-8557, June.

A model for calculating the reaction of zirconium with steam according to the Cathcart-Pawel correlation has been incorporated into RELAP5/MOD3. A cladding deformation model that computes swelling and rupture of the cladding according to the empirical correlations for Powers and Meyer has also been incorporated into RELAP5/MOD3. This report gives the background of the models, documents their implantation into the RELAP5 subroutines, and reports the developmental assessment done on the models.

Carter, H. R., and J. R. Gloude-mans, 1986, "MIST Test Results," *14th Water Reactor Safety Information Meeting, Gaithersburg, Maryland, October 27, 1986*, Babcock & Wilcox.

The Multiloop Integral System Test (MIST) is a part of the Integral System Test (IST) Program being sponsored by the U.S. Nuclear Regulatory Commission, Electric Power Research Institute, Babcock & Wilcox (B&W) Owners Group, and B&W. The IST Program is obtaining experimental integral system data for the B&W designed nuclear steam supply system. The data acquired from MIST will be used to benchmark system computer codes, such as RELAP5 and TRAC, against simulated small break loss-of-coolant plant transients. The paper describes the design of MIST, the test program, and the test results obtained.

Chapman, J. C., 1986, *Comparison of a RELAP5/MOD2 Posttest Calculation to the Data During the Recovery Portion of a Semiscale Single-Tube Steam Generator Tube Rupture Experiment*, NUREG/CR-4749, EGG-2474, September.

This report compares a RELAP5 posttest calculation of the recovery portion of the Semiscale MOD-2B Test S-SG-1 to the test data. The posttest calculation was performed with the RELAP5/MOD2/36.02 code without updates. The recovery procedure that was calculated mainly consisted of secondary feed and steam using auxiliary feedwater injection and the atmospheric dump valve of the unaffected steam generator (the steam generator without the tube rupture). A second procedure was initiated after the trends of the secondary feed and steam procedure had been provided by two trains of both the charging and high-pressure injection systems. The Semiscale MOD-2B configuration is a small scale (1/1705), non-nuclear, instrumented model of a Westinghouse four-loop pressurized water reactor power plant. S-SG-1 was a single-tube, cold-side, steam generator tube rupture experiment. The comparison of the posttest calculation and data included comparing the (a) general trends and the driving mechanisms of the responses, (b) the phenomena, and (c) the individual responses of the main parameters.

Chapman, J. C., 1986, *Quick Look Report for Semiscale MOD-2C Experiment S-NH-3*, EGG-RTH-7232, May.

The preliminary results of the Semiscale Test S-NH-3 are presented in this report. S-NH-3 was conducted in the Semiscale facility (MOD-2C configuration) on January 15, 1986. S-NH-3 simulated a small break loss-of-coolant accident in a pressurized water reactor with an accompanying failure of the high-pressure injection emergency core cooling system. The simulated break represented a shear of a small diameter cold leg penetration equivalent to 0.5% of the cold leg flow area. The test was initiated by opening a quick opening break valve. Only the automatic safety features (with the exception of the high-pressure injection) were simulated until the heater rod peak cladding temperature (PCT) reached 811 K (1000°F). The intact loop pump was then restarted at its initial speed. No other simulated operator actions were taken until the PCT reached 950 K (1250°F). The atmospheric dump valves were then opened. The test was stopped after the primary pressure was reduced to the low-pressure injection system set pressure, 1.38 MPa (200 psia). The results presented include a description of the test response, a discussion of the main mechanisms that drove the response, and a comparison of the test data of the pretest planning calculation performed using RELAP5/MOD2.0.

Chapman, J. C., and R. A. Callow, 1989, *Emergency Response Guide-B ECCS Guideline Evaluation Analyses for N Reactor*, EGG-EAST-8385, July.

The Idaho National Engineering Laboratory conducted two Emergency Core Cooling System (ECCS) analyses for Westinghouse Hanford. Both analyses will assist in the evaluation of proposed changes to the N Reactor Emergency Response Guide-B ECCS guideline. The analyses were a sensitivity study for reduced-ECCS flow rates and a mechanically determined confinement steam source for a delayed-ECCS loss-of-coolant accident (LOCA) sequence. The reduced-ECCS sensitivity study established the maximum allowable reduction in ECCS flow as a function of time after core refill for a large break LOCA sequence in the N-Reacto. The maximum allowable ECCS flow reduction is defined as the maximum flow reduction for which ECCS continues to provide adequate core cooling. The delayed ECCS analysis established the liquid and steam break flows and enthalpies during the reflood of a hot core following a delayed ECCS injection LOCA sequence. A simulation of a large hot leg manifold break with a seven-minute ECCS injection delay was used as a representative LOCA sequence. Both analyses were performed using the RELAP5/MOD2.5 transient computer code.

Chauliac, D., Y. Kukita, M. Kawaji, H. Nakamura, and K. Tasaka, 1988, *Post-Test Analysis with RELAP5/MOD2 of ROSA-IV/LSTF Natural Circulation Test ST-NC-02*, October 1988, CEA Centre d'Etudes Nucleaires de Fontenay-aux-Roses, 92, France, Japan Atomic Energy Research Institute Tokyo.

Results of posttest analysis for the ROSA-IV/LSTF natural circulation experiment ST-NC-02 are presented. The experiment consisted of many steady-state stages registered for different primary inventories. The calculation was done with RELAP5/MOD2/36.00. Discrepancies between the calculation and the experiment are (a) the core flow rate is overestimated at inventories between 80% and 95% and (b) the inventory at which dryout occurs in the core is also greatly overestimated. The causes of these discrepancies were studied through sensitivity calculations. The following key parameters are pointed out: the interfacial friction and form loss coefficients in the vessel riser, the steam generator (SG)

U-tube multidimensional behavior, and the interfacial friction in the SG inlet plenum and in the pipe below.

- Chen, T. H., and T. J. Boucher, 1985, "Semiscale Steam Line Break Transient Test Predictions with the RELAP5/MOD2 Code," *American Nuclear Society Winter Meeting, San Francisco, California, November 1985, Transactions of the American Nuclear Society, Vol. 50, pp. 327-329.*

Although ruptures of steam generator main steam lines are not expected to occur often in pressurized water reactor (PWR) plants, the potential consequences of these events necessitate their examination. Steam line break transients can lead to overcooling and possibly repressurization of the primary coolant system. This phenomenon, termed pressurized thermal shock, poses a threat to the integrity of the PWR pressure vessel. This paper presents the analysis of test data and compares the data with the pretest calculations results for the first Semiscale steam line break test (FS-2) performed in the Semiscale MOD-2C facility. Most of the primary and secondary responses including the overcooling and depressurization of the primary system were reasonably well predicted by RELAP5/MOD2, although a difference was noted in the primary coolant temperature...

- Choi, J. H., S. Y. Lee, and K. I. Han, 1988, "Core Channel Modeling for PWR LOCA Analysis," *Third International Topical Meeting on Nuclear Power Plant Thermal Hydraulics and Operations, Seoul, Korea, November 1988, Korea Advanced Energy Research Institute.*

Flow distributions are predicted in average and hot channels of the reactor core during small break loss-of-coolant accidents (LOCAs). The effects that crossflow between two channels has on LOCA analysis results are also estimated based on RELAP5/MOD2 calculations. Generally, it has been accepted that a single average channel is sufficient for small break LOCA core hydraulic modeling. However, based on these calculation results, hot channel modeling (two channel modeling) is necessary to guarantee more reliable and conservative results.

- Choi, H. R., Y. H. Ryu, K. I. Han, 1988, "Impact of Safety Injection Flow Rate on Small Break LOCA Behavior," *Third International Topical Meeting on Nuclear Power Plant Thermal Hydraulics and Operations, Seoul, Korea, November 1988, Korea Advanced Energy Research Institute.*

This paper investigates the effect of change in safety injection flow rate on smallbreak loss-of-coolant accident behavior. A series of calculations for different break sizes is performed using RELAP5/MOD2 based on conservative initial and boundary conditions. Also studied is the effect of break size changes with a given safety injection flowrate assumption to determine the limiting break size. From the calculation results, it is concluded that the degree of the peak clad temperature (PCT) increase is mostly affected by the duration of core heatup. Higher safety injection flow tends to shorten the duration of the core heatup, which results in a decrease of PCT for a given break size. It is also noted that the limiting break size tends to increase as the safety injection flowrate increases while reducing PCT.

Chow, H., and V. H. Ransom, 1984 "A Simple Interphase Drag Model for Numerical Two-Fluid Modeling of Two-Phase Flow Systems," *Transactions of the American Nuclear Society 2:3 Proceedings of Nuclear Thermal-Hydraulics, New Orleans, Louisiana, June 1984, Vol. 46.*

The interphase drag model that has been developed for RELAP5/MOD2 is based on a simple formulation having flow regime maps for both horizontal and vertical flows. The interphase drag model is based on a conventional empirical formulation that includes the product of drag coefficient, interfacial area, and relative dynamic pressure. The drag coefficient and interfacial area density are functions of the component orientation, flow regime, and local fluid properties. The flow regime maps contain those regimes of importance in light water reactor safety transient analysis and are based on recent research results that have been obtained in the U.S. Nuclear Regulatory Commission's Safety Research Program. The interphase drag model is implemented in the RELAP5/MOD2 light water reactor transient analysis code and has been used to simulate a variety of separate effects experiments to assess the model accuracy. Results are presented and discussed from three of these simulations: the General Electric Company small vessel blowdown experiment, Dukler and Smith's counter-current flow experiment, and a Westinghouse Electric Company FLECHT-SEASET forced reflood experiment.

Coney, M., and I. Brittain, 1989, "TRAC and RELAP5 Code Development within the UK," *16th Water Reactor Safety Information Meeting, Gaithersburg, Maryland, March 1989*, (United Kingdom Atomic Energy Authority, Winfrith, England).

The United Kingdom (UK) is using the TRAC-PF1 code to assess licensing calculations for large break loss-of-coolant accidents (LOCAs) in pressurized water reactors. The RELAP5 code is being used for small LOCAs and pressurized transients. The UK has participated in the International Code Assessment and Applications Program (ICAP) with respect to the assessment of TRAC-PF1/MOD1 and RELAP5/MOD2, and some work is still ongoing in this area. Since January 1988, the UK has also been collaborating with other ICAP members on the Code Improvement Plan, which seeks to remedy some of the code deficiencies identified in the assessment work. The contribution to the Code Improvement Plan is in the three areas. The largest effort is directed at the problem of post-critical heat flux heat transfer and quenching. Although it is hoped that the proposed improvements will be adopted for both codes, the UK effort is aimed at implementation in the TRAC code, since this is seen mainly as a large LOCA phenomenon. The second area of UK involvement is that of interphase drag under wet wall conditions. The main purpose of this work is to obtain improved predictions of voidage and level swell in rod bundles, particularly during small break LOCAs. The UK implementation is therefore aimed at RELAP5 for this case. The third area is the implementation of an improved off-take model to make more accurate predictions of the flow and quality from a junction or break in a horizontal pipe (e.g. the PWR hot leg), where stratified conditions might exist. The paper describes the work in progress in the UK relating to these three areas.

Coxford, M. G., and P. C. Hall, 1989, *Analysis of the THETIS Boildown Experiments Using RELAP5/MOD2*, July 1989, Central Electricity Generating Board, Barnwood, United Kingdom.

To test the ability of RELAP5/MOD2 to model two-phase mixture level and fuel rod heat transfer when the core has become partially uncovered, posttest calculations have been carried out of a series of boildown tests in the AEEW THETIS out-of-pile test facility. This report describes the comparison between the code calculations and the test data. Excellent agreement is obtained with mixture level boildown rates in tests at pressures of 40 bar and 20 bar. However, at pressures below 10 bars, the boildown rate is considerably overpredicted. A general tendency for RELAP5/MOD2 to overpredict void fraction below the two-phase mixture level is observed and is traced to defects in the interphase drag models within the code. The heat up of exposed rods above the two-phase mixture level is satisfactorily calculated by the code. The results support the use of RELAP5/MOD2 for analysis of high-pressure core boildown events in pressurized water reactors.

Cozzuol, J. M., 1988, *Loss-of-Pumping Accident in Savannah River L-Reactor*, EGG-EAST-8273, October.

An analysis of a loss-of-pumping accident has been performed using a RELAP5 model of the Savannah River L-Reactor plant. The analysis showed that the loss-of-pumping accident transient was characterized by an early process system cooldown resulting from reactor trip, followed by a heatup and rapid expulsion of process system coolant once pump availability was lost. Approximately 25,000 kg of coolant left the process system through the supplementary pressure relief system flow path during the period of expulsion. The expulsion of coolant led to a much earlier dryout and heatup of reactor fuel than would be expected from a simple boiloff. Cladding temperature in the peak power region of the core reached 600°C by about 750 seconds.

Cozzuol, J. M., and C. B. Davis, 1989, *Description of the Two-Loop RELAP5 Model of the L-Reactor at the Savannah River Site*, EGG-EAST-8449, December.

A two-loop RELAP5 input model of the L-Reactor at the Savannah River Site (SRS) was developed to support thermal hydraulic analysis of SRS reactors. The model was developed to economically evaluate potential design changes. The primary simplifications in the model were in the number of loops and the detail in the moderator tank. The six loops in the reactor were modeled with two loops, one representing a single loop and the other representing five combined loops. The model has undergone a quality assurance review. This report describes the two-loop model, its limitations, and quality assurance.

Davis, C. B., 1989, *A Comparison of RELAP5 and TRAC LOCA Calculations for the K-14.1 Charge at SRS*, EGG-EAST-8608, August.

Calculations of a loss-of-coolant accident (LOCA) in K-Reactor at the Savannah River Site were performed using the RELAP5 computer code. The results of the RELAP5 calculation were then compared with a TRAC calculation previously performed by Savannah River Laboratory. The calculations represented the early (flow instability) portion of a LOCA initiated by a double-ended guillotine break in the plenum inlet piping in K-Reactor. A RELAP5 model of K-Reactor was developed to perform the calculations. The model represented all six external loops and represented the reactor vessel in a three-dimensional manner. The RELAP5 and TRAC results were compared to illustrate



and understand differences and similarities between calculations performed with independent computer codes and input models. The variation between the independent calculations provided an indication of the uncertainty in the calculated results with both codes. Results of the comparison were generally favorable because differences between the calculated results for the water plenum and tank bottom pressures were generally less than the values currently assumed in Savannah River's FLOWTRAN uncertainty studies.

Davis, C. B., 1988, *Pump Cavitation in L-Reactor During a LOCA Initiated by a Large Break in a Plenum Inlet Line*, EGG-FAST-8148, June.

This study analyzed the effects of cavitation on the response of L-Reactor at Savannah River during a loss-of-coolant accident (LOCA) initiated by a large break in a plenum inlet line. Cavitation models were developed and incorporated into a RELAP5/MOD2 model of L-Reactor. The types of cavitation modeled include elbow cavitation and pump cavitation.

The RELAP5 cavitation models were benchmarked against separate-effects and system data. The RELAP5 model of L-Reactor was benchmarked against steady state data and LOCA calculations performed with other computer codes. The results of the benchmark comparisons were generally favorable.

Calculations of a LOCA initiated by a 200% plenum inlet break were performed at pre-incident core power levels of 1125, 1400, 1800, and 2250 MW. Based on a best-estimate analysis and an average river water temperature of 18°C, the power required to cause cavitation was shown to be in excess of current operating powers. The analysis showed that even though cavitation would occur during a LOCA if the initial core power was high enough, a catastrophic reduction in assembly flow would not occur because of system feedback, which would limit the effects of cavitation.

Davis, C. B., 1987, *Davis-Besse Uncertainty Study*, NUREG/CR-4946, EGG-2510 August.

The uncertainties of loss-of-feedwater transient calculations at Davis-Besse Unit 1 were determined to address concerns of the U.S. Nuclear Regulatory Commission relative to the effectiveness of feed and bleed cooling. Davis-Besse Unit 1 is a pressurized water reactor of the raised-loop Babcock and Wilcox design. A detailed, quality-assured RELAP5/MOD2 model of Davis-Besse was developed at the Idaho National Engineering Laboratory. The model was used to perform an analysis of the loss-of-feedwater transient that occurred at Davis-Besse on June 9, 1985. A loss-of-feedwater transient followed by feed and bleed cooling was also calculated. The evaluation of uncertainty was based on the comparisons of calculations and data, comparisons of different calculations of the same transient, sensitivity calculations, and the propagation of the estimated uncertainty in initial and boundary conditions to the final calculated results.

Davis, C. B., C. D. Fletcher, and S. B. Rodriguez, 1989, *Benchmarking the RELAP5 L-Reactor Model with Savannah River Reactor Test Data*, EGG-EAST-8336, April.

A quality-assured RELAP5 input model of the L-Reactor at the Savannah River Plant (SRP) was developed to support the analysis of a loss-of-coolant accident. The

RELAP5/MOD2.5 computer code and the L-Reactor model were benchmarked against SRP data to demonstrate their applicability for thermal hydraulic analysis of SRP reactors. The code and model were benchmarked against data from several different reactor system tests including the 1985 AC Process Flow Tests, the 1983 Cavitation Tests, the 1987 AC Pump Trip Tests, and the 1970 Starved Pump Tests. Results of the benchmark calculations were favorable, yielding confidence in the capability of RELAP5 and the L-Reactor model to determine system response during normal and transient operation, including a loss-of-coolant accident.

DeForest, D. L., and Y. A. Hassan, 1987, "RELAP5/MOD2 Implementation on Various Mainframes Including the IBM and SX-2 Supercomputer," *Transactions of the American Nuclear Society*, 55, pp. 709-710.

The results obtained with RELAP5/MOD2/36.04 from various simulations are of interest to many utilities involved in licensing and evaluating nuclear power plants. Typically, there is a limit in the number and scope of simulation because of computational time, expense, and availability restraints. Thus, efforts have been made to install RELAP5 on additional computer systems that improve speed and/or availability. From the original Control Data Corporation (CDC) version of RELAP5/MOD2 came the operational version on the CRAY supercomputers. The purpose of this work is to install and benchmark the RELAP5/MOD2 code on an Amdahl V8/460 (IBM look-alike) and IBM 3090-200E with vector facility located at Texas A&M University, and the NEC SX-2 supercomputer located at the Houston Area Research Center. The SX-2 is the first Japanese supercomputer to be installed in the United States. At Texas A&M, the latest version of RELAP5/MOD2/36.04 has been installed for the first time in the United States on an IBM environment and on the NEC SX-2 supercomputer. Results from benchmark runs demonstrate capabilities comparable to installation on a CDC mainframe and the CRAY supercomputers, respectively.

Dillistone, M. J., and C. G. Richards, 1988, *Modeling Vertical Counter-Current Flow Limitation Using RELAP5/MOD2*, PWR/HTWG/P(88)606, AEEW-M 2512, May, AEE Winfrith, United Kingdom.

An experiment to investigate counter-current flow limitation in a vertical pipe has been modelled using the thermal hydraulics code RELAP5/MOD2/36.05. The RELAP5 code has been used to generate a curve representing the maximum liquid downflow in a pipe for a given steam upflow, known as the flooding curve. This curve is compared with experimental data. The code overpredicts liquid downflows by more than an order of magnitude, and this is shown to be mainly from an undocumented code model (the Reverse Void Profile model) that reduces interphase friction when fluid density increases with height in a vertical section.

With the model removed, the code still overpredicts liquid downflows at lower gas flow rates because it assumes slug flow in the channel when annular flow is appropriate (the co-current flow-regime transition criterion applied is inappropriate in a counter-current flow situation). The code reproduces the experimental flooding-curve well at all gas flow rates if it is forced to assume annular flow in the channel. The effect of varying the number of

mesh cells representing the test-section is also discussed. The code also predicts greater liquid downflows than are theoretically allowed by the balance between interphase drag and gravity forces. This is due in part to the upstream donoring of voids at junctions, and in part to another component of the Reverse Void Profile model.

Dobbe, C. A., and R. Chambers, 1984, *Analysis of a Station Blackout Transient for the Bellefonte Pressurized Water Reactor*, EGG-NTP-6704, October.

Analyses of a station blackout transient in support of the U.S. Nuclear Regulatory Commission's Severe Accident Sequence Analysis Program are presented. The RELAP5/MOD2 and SCDAP/MOD1 computer codes were used to calculate the effects of concurrent loss of offsite power, onsite power, and emergency feedwater during full power operation on the Bellefonte Babcock and Wilcox designed pressurized water reactor. The results were calculated from transient initiation through severe core damage. Results provide insight into timing significant events and the severity of core damage.

Dobbe, C. A., P. D. Bayless, and R. Chambers, 1985, "Analysis of Feedwater Transient Initiated Sequences for the Bellefonte Nuclear Plant," *13th Water Reactor Safety Information Meeting, Washington, D.C., October 1985*, EGG-M-21285.

Four feedwater transient-initiated sequences for the Bellefonte Nuclear Plant were analyzed. The sequences were evaluated to determine if core damage would result. Calculations were performed with the RELAP5/MOD2 computer code until either cladding oxidation or long term core cooling was obtained. The analyses show that a total loss of power and auxiliary feedwater (TMLB' sequence) results in core damage. The addition of a single high-pressure injection pump provided adequate core cooling.

Driskell, W. E., and R. G. Hanson, 1989 "Summary of ICAP Assessment Results for RELAP5/MOD2," *Nuclear Safety*, 30, 3.

The International Code Assessment and Applications Program (ICAP) encompasses bilateral agreements between the U.S. Nuclear Regulatory Commission and fourteen nations and/or multinational organizations. One purpose of ICAP is to provide assessments of the RELAP5 computer code to identify code deficiencies and draft user guidelines. To date, twenty assessment studies have been provided by ICAP assessing the RELAP5/MOD2 code. Of these, ten have been reviewed and evaluated. Based on these ten studies, three code deficiencies were identified and four user guidelines drafted. The code deficiencies are listed and the user guidelines stated. A summary of the information considered and the procedure used in the identification of the code deficiencies and the formulation of user guidelines is given.

Duffley, R. B., 1988, "The Analysis of Plant Transients Defines Safety Margins and Accident Management Strategies," *Third International Topical Meeting on Nuclear Power Plant Thermal Hydraulics and Operations, Seoul, Korea, December 1988*.

Developments in system analysis and simulation are described that cover the application to training, uncertainty determination, survivability, and accident management.

Eriksson, J., 1989, *Assessment of RELAP5/MOD2 Cycle 36.04 Against FIX-II Guillotine Break Experiment No. 5061*, July, Swedish Nuclear Power Inspectorate, Stockholm, Sweden.

The FIX-II guillotine break experiment No. 5061 has been analyzed using RELAP5/MOD2 (frozen version 36.04). Four different calculations were carried out to study the sensitivity of initial coolant mass, junction options, and break discharge line nodalization. The differences between the calculations and the experiment have been quantified over intervals in real time for a number of variables available from the measurements during the experiment. The break mass flows were generally underpredicted at the same time the depressurization rate was overpredicted.

Eriksson, J., 1987, *ICAP Assessment of RELAP5/MOD2, Cycle 36.04 Against LOFT Small Break Experiment L3-6*, STUDSVIK/NP-37/128, Project 850026, Reference 13.3-717/84, November 3, Swedish Nuclear Power Inspectorate.

The LOFT small break experiment L3-6 has been analyzed as part of Sweden's contribution to the International Code Assessment and Applications Program. Three calculations, of which two were sensitivity studies, were carried out. Two quantities were varied: the content of secondary side fluid and the feed water valve closure, and the two-phase characteristics of the main pumps.

All three predictions agreed reasonably well with most of the measured data. The sensitivity calculations resulted only in marginal improvements. The predicted and measured data are compared on plots, and their differences are quantified over intervals in real time.

Eriksson, J., 1986, *ICAP Assessment of RELAP5/MOD2 Cycle 36 Against FIX-II Split Break Experiment No. 3027*, NUREG/IA-0005, September.

The FIX-II split break experiment No. 3027 has been analyzed using the RELAP5/MOD2 (frozen version 36). Four different prediction calculations were carried out to study the sensitivity of various parameters to changes of break discharge, initial coolant mass, and passive heat structures. The differences between the calculations and the experiment have been quantified over intervals in real time for a number of variables available from the measurements during the experiment. The core inventory expressed by the differential pressure over the core was generally underpredicted. Dryout times were generally overpredicted, probably because of differences in the used dryout correlation.

NOTE: This report is restricted to International Code Assessment Program members unless specific permission is granted by the author.

Fineman, C.P., 1986, "RELAP5/MOD2 Code Assessment for the Semiscale Mod-2C Test S-LH-1," *Proceedings of the International ANS/ENS Topical Meeting on Thermal Reactor Safety, San Diego, California, February 2, 1986*.

RELAP5/MOD2,36.02 was assessed using data from Semiscale MOD-2C Experiment S-LH-1. The major phenomena that occurred during the experiment were calculated by



RELAP5/MOD2, although the duration and magnitude of their effect on the transient were not always well calculated. Areas defined where further work was needed to improve the RELAP5 calculation include (a) the system energy balance, (b) core interfacial drag, and (c) the heat transfer logic rod dryout criterion.

Fisher, J. E., 1990, *Savannah River Site Reactor Hardware Design Modification Study*, EGG-EAST-8984, April.

A study was completed to assess the merits of proposed design modifications to the Savannah River Site reactors. The evaluation was based on the responses calculated by the RELAP5 systems code to double-ended guillotine break loss-of-coolant accidents. The three concepts evaluated were (a) elevated plenum inlet piping with a guard vessel and clamshell enclosures, (b) closure of both rotovalves in the affected loop, and (c) closure of the pump suction valve in the affected loop. Each concept included a fast reactor shutdown (to 65% power in 100 ms) and a 2-s ac pump trip. For the elevated piping design, system recovery was predicted for breaks in the plenum inlet, or pump suction piping response to the pump discharge break location did not show improvement compared to the present system configuration. The rotovalve closure design improved system response to plenum inlet or pump discharge breaks; recovery was not predicted for pump suction breaks. The pump suction valve closure design demonstrated system recovery for all break locations. The elevated piping design performance during pump discharge breaks would be improved with the addition of a dc pump trip in the affected loop. Valve closure design performance for a break location in the short section of piping between the reactor concrete shield and the pump suction valve would benefit from the clamshell enclosing that section of piping.

Fletcher, C. D., et. al., 1985, *RELAP5 Thermal-Hydraulic Analyses of Pressurized Thermal Shock Sequences for the H. B. Robinson Unit Pressurized Water Reactor*, NUREG/CR-3977, EGG-2341, April.

Thermal hydraulic analyses of fourteen hypothetical pressurized thermal shock (PTS) scenarios for the H. B. Robinson, Unit 2 pressurized water reactor were performed at the Idaho National Engineering Laboratory using the RELAP5 computer code. The scenarios, which were developed at Oak Ridge National Laboratory (ORNL), contain significant conservatisms concerning equipment failures, operator actions, or both. The results of the thermal hydraulic analyses presented here, along with additional analyses of multidimensional and fracture mechanics effects, will be used by ORNL, integrator of the PTS study, to assist the U. S. Nuclear Regulatory Commission in resolving the PTS unresolved safety issue.

Fletcher, C. D., and M. A. Bolander, 1988, *N Reactor RELAP5 Model Benchmark Comparisons*, EGG-TFM-7938, December.

This report documents work performed at the Idaho National Engineering Laboratory (INEL) in support of Westinghouse Hanford Company safety analyses for N-Reactor. The portion of the work reported here includes comparisons of RELAP5/MOD2-calculated data with measured plant data for (a) a plant trip reactor transient from full power operation,



and (b) a hot dump test performed before plant startup. These qualitative comparisons are valuable because they show the capabilities of the RELAP5/MOD2 model and code to simulate operational and blowdown transients in N-Reactor.

Fletcher, C. D., and M. A. Bolander, 1986, *Analysis of Instrument Tube Ruptures in Westinghouse 4-Loop Pressurized Water Reactors*, NUREG/CR-4672, EGG-2461, December.

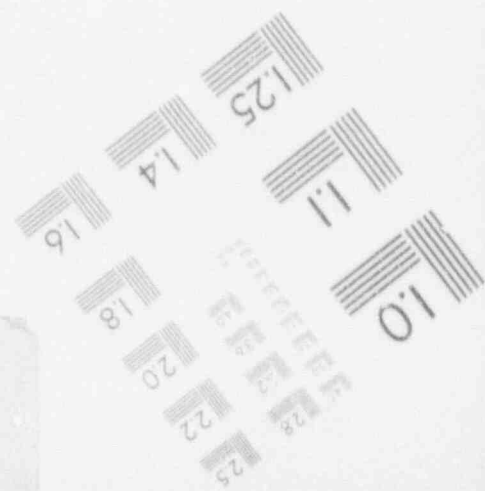
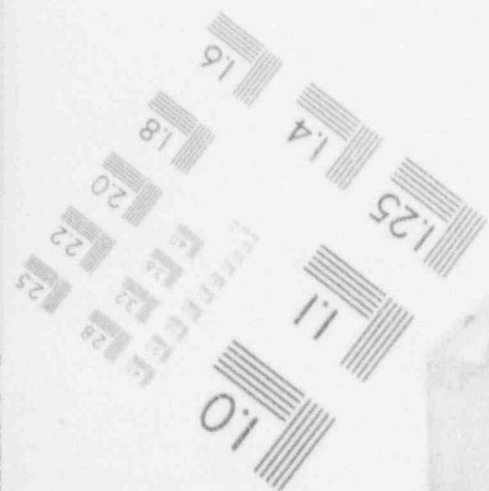
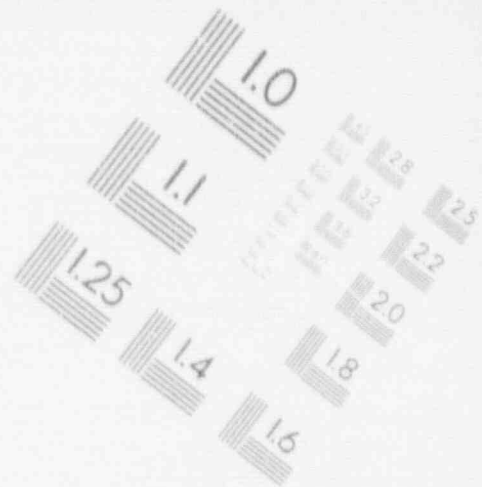
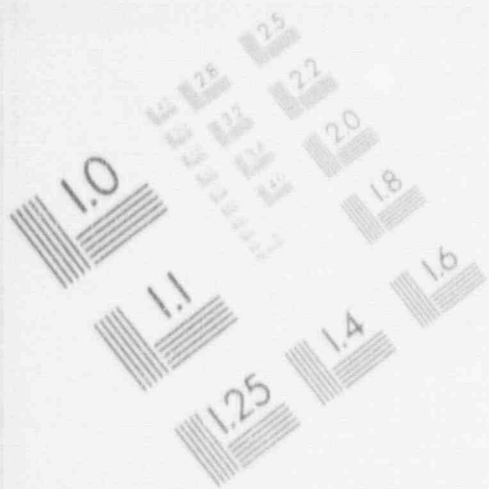
A recent safety concern for Westinghouse 4-loop pressurized water reactors (PWRs) is that, because of a seismic event, instrument tubes may be broken at the flux mapping seal table, resulting in an uncovering and heatup of the reactor core. This study's purpose was to determine the effects on findings of a similar 1980 study if certain test variables changed. A 1980 U. S. Nuclear Regulatory Commission analysis of PWR behavior used the RELAP4/MOD7 computer code to determine the effects of breaking instrument tubes at the reactor vessel lower plenum wall. The 1986 study discussed here was performed using RELAP5/MOD2, an advanced best-estimate computer code. Separate effects analyses investigated instrument tube pressure loss, heat loss, and tube nodalization effects on break flow. Systems effects analyses (a) investigated the effects of changing the break location from the reactor vessel to the seal table, (b) compared RELAP4/MOD7 and RELAP5/MOD2 results for an identical transient, (c) verified a key finding from the 1980 analysis, and (d) investigated instrument tube ruptures in the Zion-1 FWR using best-estimate boundary and initial conditions. The outcome of these analyses permits adjustment of the 1980 analysis findings for instrument tube ruptures at the seal table and indicates the best-estimate response of a Westinghouse PWR to the rupture of 25 small instrument tubes at the seal table.

Fletcher, C. D., and R. A. Callow, 1988, *Long Term Recovery of Westinghouse Pressurized Water Reactors Following a Large Break Loss of Coolant Accident*, EGG-TFM-7993, February.

The U.S. Nuclear Regulatory Commission recently identified a possible safety concern. Following the reflood phase of a large break loss-of-coolant accident in pressurized water reactors of Westinghouse design, long term cooling of the reactor core may not be ensured. The specific concern is that the loop seals in the reactor coolant pump suction piping will refill with liquid and the post-reflood steam production may depress the liquid levels in the downflow sides of the loop seals, causing a corresponding depression of the core liquid levels and a possible fuel rod heatup in the upper core region. This report documents analyses of the loop seal/core level depression issue performed at the Idaho National Engineering Laboratory. The analyses employed both a static-balance, steady-state approach, and a transient system approach. The static balance approach involved the development and application of a simple computer program to investigate the reactor coolant system behavior during quiescent post-reflood conditions. The transient systems approach involved investigating this behavior using the RELAP5/MOD2 computer code and a comprehensive RELAP5 model of a Westinghouse pressurized water reactor. Two approaches were used because of uncertainties regarding the actual reactor coolant system behavior during the post-reflood period. The static balance analysis indicated a fuel rod heatup is possible, but not to temperatures that could damage the fuel rods. The transient systems analysis indicated boiling and condensation-induced flow oscillations, not considered

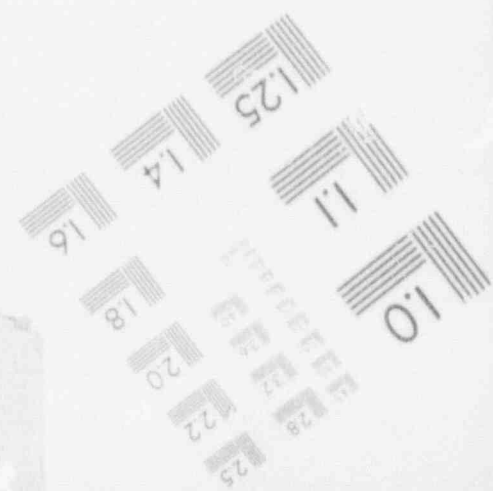
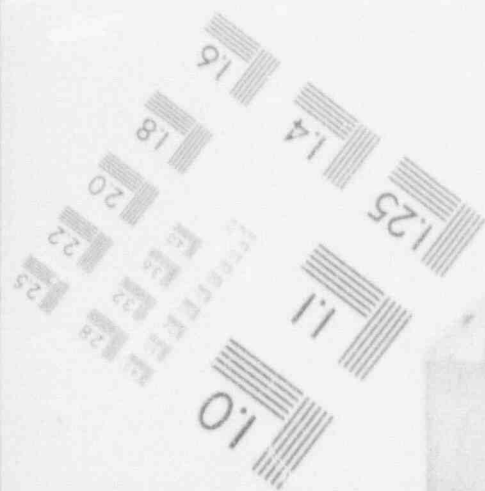
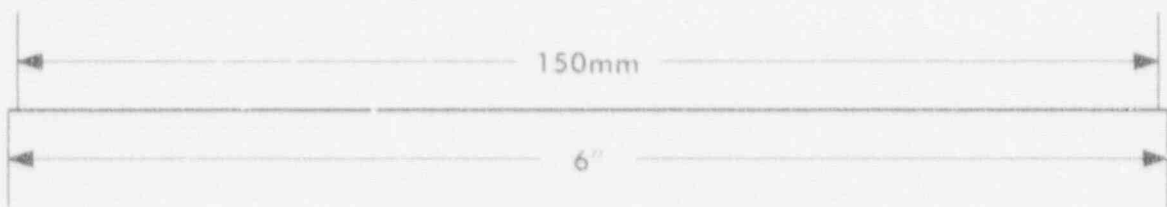
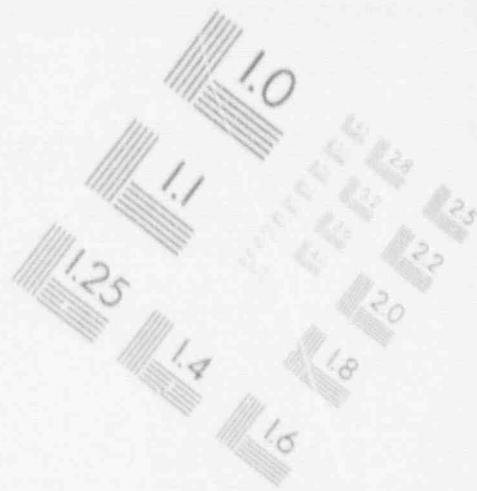
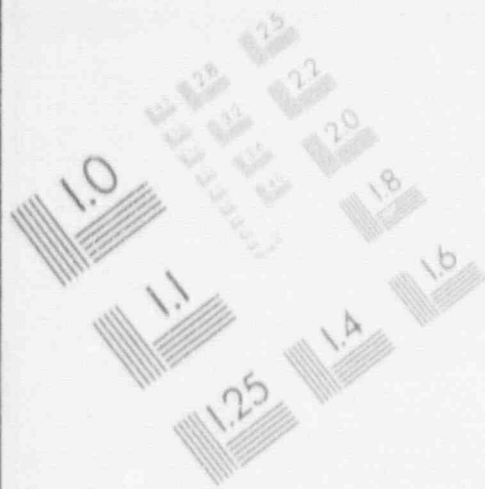
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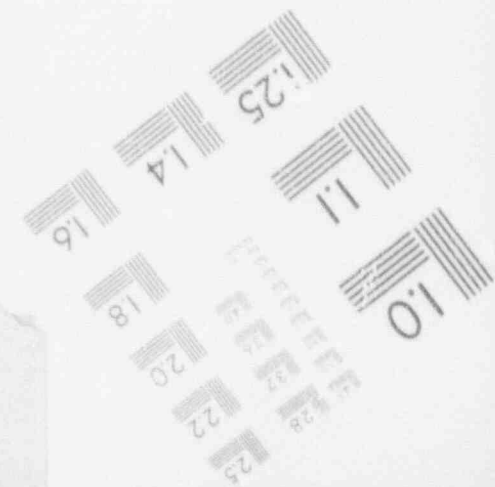
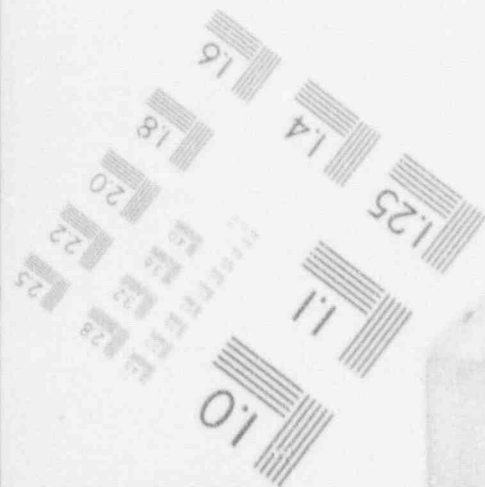
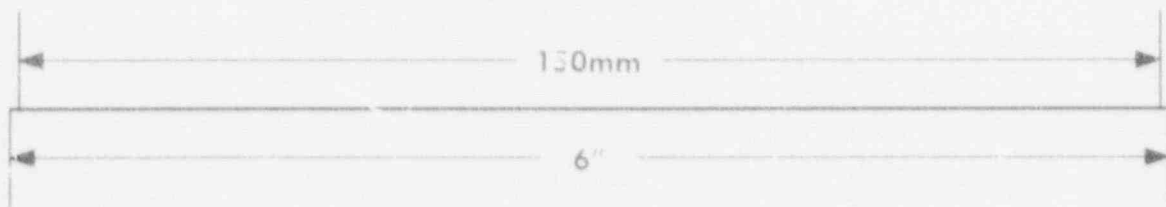
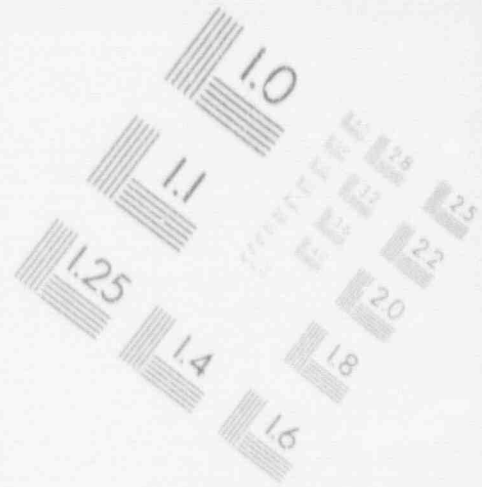
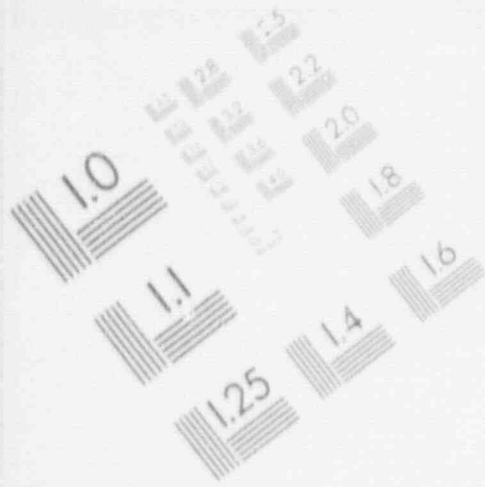
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in the static balance analysis, are sufficient to prevent fuel rod heatup. The report includes discussions of analysis uncertainties and recommendations for further work in this area.

Fletcher, C. D., and C. M. Kullberg, 1985, *Break Spectrum Analysis for Small Break Loss-of-Coolant Accidents in a RESAR-3S Plant*, NUREG/CR-4384, EGG-2416, September.

A series of thermal hydraulic analyses were performed to investigate phenomena during small break loss-of-coolant accident sequences in a RESAR-3S pressurized water reactor. The analysis included simulations of plant behavior using the TRAC-PF1 and the RELAP5/MOD2 computer codes. A series of calculations was performed using both codes for different break sizes. The results shown here were used by the U. S. Nuclear Regulatory Commission as an independent confirmation of similar analyses performed by Westinghouse Electric Company using another computer code.

Fletcher, C. D., R. Chambers, and M. A. Bolander, 1986, *Modeling and Simulation of the Chernobyl-4 Reactor Under Severe Accident Conditions*, EGG-SAR-7511, December.

RELAP5 and SCDAP computer code models of Chernobyl-4 were assembled and applied. Plant response to a station blackout event with failure of all feedwater was considered first. Immediately following the accident this was considered a possible scenario. As information on the events at Chernobyl became more available, intermediate analyses investigated the effects of the new information on plant response during the accident. Finally, following the comprehensive release of information at the International Atomic Energy Agency expert conference in Vienna, Austria, August 25-29, 1986, an analysis was performed of the accident sequence for the five-minute period immediately preceding the plant explosion.

Fletcher, C. D., C. B. Davis, and D. M. Ogden, 1985, *Thermal-Hydraulic Analyses of Overcooling Sequences for the H. B. Robinson Unit 2 Pressurized Thermal Shock Study*, NUREG/CR-3935, EGG-2335, May.

Oak Ridge National Laboratory, as part of the U.S. Nuclear Regulatory Commission's pressurized thermal shock (PTS) integration study for the resolution of Unresolved Safety Issue A49, identified overcooling sequences of interest to the H. B. Robinson PTS study. For each sequence, reactor vessel downcomer fluid pressure and temperature histories were required for the two-hour period following the initiating event. Analyses previously performed at the Idaho National Engineering Laboratory (INEL) fully investigated a limited number of the sequences using a detailed RELAP5 model of the H. B. Robinson, Unit 2 plant. However, a full investigation of all sequences using the detailed model was not economically practical. New methods were required to generate results for the remaining sequences. Pressure and temperature histories for these remaining sequences were generated at the INEL through a process combining (a) partial-length calculations using the detailed RELAP5 model, (b) full-length calculations using a simplified RELAP5 model, and (c) hand calculations. This report documents both methods used in this process and the results. The sequences investigated contain significant conservatisms concerning equipment failures, operator actions, or both. Consequently, care should be taken in applying the results presented herein without an understanding of the conservatisms and assumptions.



Fletcher, C. D., R. Chambers, M. A. Bolander, and R. J. Dallman, 1988, "Simulation of the Chernobyl Accident," *Nuclear Engineering and Design*, 105, 2, January, pp. 157-172.

An analysis of the April 26, 1986 accident at the Chernobyl-4 nuclear power plant is presented. The peak calculated core power during the accident was 550,000 MW/sub t/. The analysis provides insights that further understanding of the plant behavior during the accident. The plant was modeled with the RELAP5/MOD2 computer code using information available in the open literature. RELAP5/MOD2 is an advanced computer code designed for best-estimate thermal hydraulic analysis of transients in light water reactors. The Chernobyl-4 model included the reactor kinetics effects of fuel temperature, graphite temperature, core average void fraction, and automatic regulator control rod position. Preliminary calculations indicated that the effects of recirculation pump coastdown during performance of a test at the plant were not sufficient to initiate a reactor kinetics-driven power excursion. Another mechanism, or "trigger" is required. The accident simulation assumed the trigger was recirculation pump performance degradation caused by the onset of pump cavitation. Fuel disintegration caused by the power excursion probably led to rupture of pressure tubes. To further characterize the response of the Chernobyl-4 plant during severe accidents, simulations are also presented of an extended station blackout sequence with the failure of all feedwater. For those simulations, RELAP5/MOD2 and SCDAP/MOD1 (an advanced best-estimate computer code for the prediction of reactor core behavior during a severe accident) were used. The simulations indicated that fuel rod melting was delayed significantly because the graphite acted as a heat sink.

Frei, G., T. Nguyen, G. Seeberger, K.I. Han, H.R. Choi, and Y.H. Ryu, 1988, "Application of RELAP5/MOD2 Evaluation Models for KNU Small-Break LOCA Analysis," *Third International Topical Meeting on Nuclear Power Plant Thermal Hydraulics and Operations, Seoul, Korea, November 1988*.

The small break loss-of-coolant accident (SBLOCA) analysis for a Korean Nuclear Unit is performed using RELAP5/MOD2/36.04. This paper presents results of studies of a pressurized water reactor two-loop plant SBLOCA analysis performed with the following evaluation models and key parameters: (a) gap conductance models of fuel rods, (b) critical heat flux correlations, (c) nodalization of the steam generator, and (d) noding scheme near the break and the emergency core cooling system injection point.

Gloudehans, J. R., 1991, *Multiloop Integral System Test (MIST): Final Report, Vol. 1: Summary of Key Results*, NUREG/CR-5395, April.

The Multiloop Integral System Test (MIST) was part of a multiphase program started in 1983 to address small break loss-of-coolant accidents (SBLOCAs) specific to Babcock and Wilcox designed plants. Data from MIST are used to benchmark the adequacy of system codes, such as RELAP5 and TRAC, for predicting abnormal plant transients. In 1982, a Test Advisory Group (TAG) was formed to identify experimental data needs for the Babcock and Wilcox designed nuclear steam system. The TAG developed a list of 17 issues perceived both to lack experimental data and to be of sufficient interest that such data were needed. The issues were grouped under four major topics: natural circulation, SBLOCAs,

feed and bleed, and steam generator tube rupture. The MIST facility was scaled, designed, and tested to address these issues. The MIST tests addressed each of the 17 TAG issues. A wealth of consistent integral system data have been generated for each issue. An important issue under the topic of natural circulation was the ability of boiler-condenser mode natural circulation to remove core heat and effectively depressurize the reactor coolant. In this program, the viability of this mode of primary-to-secondary heat transfer was repeatedly observed. When the prerequisite conditions for boiler-condenser mode were met, the primary system tended to depressurize through vapor condensation and the accompanying primary-to-secondary heat transfer. The ability of the reactor vessel vent valves to augment primary system depressurization during the simulated SBLOCAs was also observed in MIST. MIST repeatedly exhibited system resiliency to impose changes in the primary boundary conditions as a result of the steam venting capabilities of the reactor vessel vent valves. The ability of feed and bleed cooling to provide continual core cooling as well as system cooldown and depressurization was demonstrated in MIST.

Gregoric, M., S. Petelin, B. Mavko, and L. Parzer, 1989, "Emergency Operating Procedures for SGTR Sequence," *Technical Committee/Workshop on Computer Aided Safety Analysis, Berlin German Democratic Republic, April 1989, Computer Aided Safety Analysis 1989*, Institute Jozef Stefan, Ljubljana, Yugoslavia.

Two steam generator tube rupture accidents combined with loss of all offsite power for Nuclear Power Plant Krsko were analyzed to assess the impact of sequences of auxiliary feedwater system availability. Calculations were performed with RELAP5/MOD1/25. Results show that such a combined accident can be controlled with just half of the safety systems available (design bases). Even if less than one half of the safety systems are available (beyond design bases), the accident can be controlled by timely and correct operator actions.

Hall, D. G., 1985, *Pretest Analysis Document for Test S-FS-7*, EGG-SEMI-6919, June.

This report documents the pretest calculations completed for Semiscale Test S-FS-7. This test will simulate a transient initiated by a 14.3% break in a steam generator bottom feedwater line downstream of the check valve. The initial conditions represent normal operating conditions for a Combustion Engineering, Inc. System 80 nuclear power plant. Predictions of transients resulting from feedwater line breaks in these plants have indicated that significant primary system overpressurization may occur. The results of a RELAP5/MOD2/21 code calculation indicate that the test objectives for Test S-FS-7 can be achieved. The primary system overpressurization will occur, but poses no threat to personnel or plant integrity.

Hall, D. G., 1985, *Quick Look Report for Semiscale MOD-2C Test S-FS-7*, EGG-RTH-7072, October.

Results of a preliminary analysis of the fourth test performed in the Semiscale MOD-2C Steam Generator Feedwater and Steam Line Break (FS) experiment series are presented. Test S-FS-7 simulated a pressurized water reactor transient initiated by a 14.3% break in a steam generator bottom feedwater line downstream of the check valve. With the exception

of primary pressure, the initial conditions represented the initial conditions used for the Combustion Engineering, Inc. System 80 Final Safety Analysis Report Appendix 15B calculations. The transient included an initial 926-s period in which only the response of automatic plant protection systems was simulated. This period was followed by a series of operator actions necessary to stabilize the plant. The break was then isolated and the broken loop steam generator secondary was refilled. The test results provided an evaluation of the effectiveness of the automatic responses in minimizing primary system overpressurization and operator actions in stabilizing the plant and heat transfer information under refill conditions. The data were compared with the RELAP5/MOD2 computer code, which also contributed to an evaluation of the effect of break size on primary overpressurization and primary-to-secondary heat transfer using data from other tests in the series.

Hall, D. G., and K. A. Shaw, 1985, *Pretest Analysis Document for Test S-FS-11*, EGG-SEMI-6985, June.

This report documents the pretest calculations completed for Semiscale Test S-FS-11. This test will simulate a transient initiated by a 50% break in a steam generator bottom feedwater line downstream of the check valve. The initial conditions represent normal operating conditions for a Combustion Engineering, Inc. System 80 nuclear plant. Predictions of transients resulting from feedwater line breaks in these plants have indicated that significant primary system overpressurization may occur. The results of a RELAP5/MOD2/21 calculation indicate that the test objectives for Test S-FS-11 can be achieved. The primary system overpressurization will occur but poses no threat to personnel or plant integrity.

Hall, P. C., 1990, *RELAP5/MOD2 Calculations of OECD LOFT Test LP-SB-02*, United Kingdom, NUREG/IA-0021, April.

To help assess the capabilities of RELAP5/MOD2 for pressurized water reactor fault analysis, the code is being used by the Central Electricity Generating Board to simulate several small loss-of-coolant accident (LOCA) and pressurized transient experiments in the Loss-of-Fluid Test (LOFT) experimental reactor. The present report describes an analysis of small LOCA test LP-SB-02, which simulated a 1% hot leg break LOCA in a pressurized water reactor, with delayed tripping of the primary coolant pumps. This test was carried out under the Organization for Economic Cooperation and Development/LOFT Program.

An important deficiency identified in the code is inadequate modeling of the quality of the fluid discharged from the hot leg into the break pipework. This gives rise to large errors in the calculated system mass inventory. The effect of using an improved model for vapor pull-through into the break is described. A second significant code deficiency identified is the failure to predict the occurrence of stratified flow in the hot leg at the correct time in the test. It is believed that this error contributed to the gross errors in the loop flow conditions after about 1300 seconds. Additional separate effects data necessary to resolve the code deficiencies encountered are identified.

Hall, P. C., and G. Brown, 1986, *RELAP5/MOD2 Calculations of OECD-LOFT Test LP-SB-01*, GD/PE-N/544 (Rev.), November, Central Electricity Generating Board, Barnwood, United Kingdom.

To assist the Central Electricity Generating Board in assessing the capabilities and status of RELAP5/MOD2, the code has been used to simulate small break loss-of-coolant accident test LP-SB-01 carried out in the Loss-of-Fluid-Test (LOFT) experimental reactor under the Organization for Economic Cooperation and Development LOFT program. This test simulated a 1.0% hot leg break in a pressurized water reactor, with early tripping of the primary coolant circulating pumps. This report compares the results of the RELAP5/MOD2 analysis with experimental measurements.

Harwood, C., and G. Brown, 1986, *RELAP5/MOD2 Calculation of OECD-LOFT Test LP-SB-03*, GD/PE-N/535 (Rev), ICAP Number 00047, NUREG/IA-0013 (Central Electricity Generating Board, Barnwood United Kingdom).

This report compares the results of the RELAP5/MOD2 analysis with experimental measurements. A simulation of test LP-SB-03 was previously carried out at the Generation Development Construction Division using RELAP5/MOD1 and contains more sophisticated hydraulic models and constitutive relationships. Comparison of the RELAP5/MOD2 and MOD1 calculations show that RELAP5/MOD2 performs better than RELAP5/MOD1 in a number of key areas greatly reduced mass errors, improved numerical stability, and improved separator modeling and modeling of accumulator injection.

Hassan, Y. A., 1987, *Assessment of a Modified Interfacial Drag Correlation in Two-Fluid Model Codes*, Dallas, Texas, June 1987, CONF-870601.

Analysis of low flooding rate experiments and a number of boil-off experiments with the RELAP5/MOD2 computer code has shown that the code underpredicts the collapsed liquid level and, consequently, overpredicts the liquid carryover. Recent analyses using several other codes (e.g., TRAC-BD1 and the French code CATHARE) have also resulted in the underprediction of collapsed liquid level histories. The discrepancy between the measurements and code predictions is attributed to the interfacial drag between the phases. A new interfacial drag formulation in the bubbly/slug flow regimes is incorporated in the RELAP5/MOD2 code. Better agreement with the measurements is obtained.

Hassan, Y. A., 1986, "Analysis of FLECHT and FLECHT-SEASET Reflood Tests with RELAP5/MOD2," *Nuclear Safety Magazine*, February.

Overall, the RELAP5/MOD2 reflux heat transfer package has demonstrated promising capabilities in predicting the behavior of FLECHT and FLECHT-SEASET unblocked flow tests. In general, the correct qualitative system behavior was predicted. The predictions for the steam cooling test and the high flooding rate test are in good agreement with the measurements in the low flooding case. The major shortcomings of RELAP5/MOD2 are its tendencies to predict lower temperatures and unrealistic void fraction oscillations with low flooding rate test cases. The spikes in void fraction histories were flow-regime dependent and traced to discontinuities in interfacial drag models. From the results, it is clear that the

interfacial drag model at the quench front needs to be refined to achieve accurate results during reflood.

Hassan, Y. A., 1986, "Dispersed-Flow Heat Transfer During Reflood in a Pressurized Water Reactor After a Large-Break Loss-of-Coolant Accident," *American Nuclear Society and Atomic Industrial Forum Joint Meeting, Washington, D. C., November 1986.*

The postulated loss-of-coolant accident (LOCA) of a pressurized water reactor has been the subject of intensive experimental and analytical studies in light water reactor safety analysis. Many efforts are devoted to the investigation of the thermodynamic behavior of the reactor core and the effectiveness of the emergency core cooling system during the reflood phase of a LOCA. In the initial period of reflood phase, the flow patterns at the core higher elevation are considered as the dispersed flow regime. The effect of liquid phase on the heat transfer cannot be neglected in this dispersed flow regime. It has been found experimentally that a steam-water-droplet flow is ultimately responsible for terminating the cladding temperature excursions in a LOCA. Recently, a study of reflood test predictions with RELAP5/MOD2 showed a tendency to predict lower cladding temperatures during the dispersed flow regime. The purpose of this study is to present a new dispersed flow film boiling implemented in RELAP5/MOD2. In addition, RELAP5 underestimated the vapor temperature. Therefore, a revised interfacial heat transfer coefficient between the droplets and steam was incorporated in the code. Comparison of the current predicted cladding/fuel temperature histories with the reflood data showed a fair agreement.

Hassan, Y. A., 1986, "Modifications and Assessment of Rewetting Correlations for Light Water Reactor System Analysis," *American Nuclear Society and Atomic Industrial Forum Joint Meeting, Washington, D. C., November 1986.*

The qualitative aspects of reflood heat transfer in the system codes (e. g., RELAP5/MOD2, TRAC-PF1/MOD1, COBRA-TF) can be represented with a generalized boiling curve. The anchor points used to specify the boiling curve are the critical heat flux (CHF) temperature ( $T_{\text{sub CHF}}$ ) and the minimum flow boiling temperature ( $T_{\text{sub min}}$ ). The cooldown during the quenching process is affected by the minimum film boiling heat flux. This aspect of the quenching process has not been studied as much as the CHF phenomenon. The purpose of this paper is to compare several rewetting correlations. These correlations were implemented in a special version of RELAP5/MOD2. Good agreement between several FLECHT-SEASET data and predicted rewetting temperatures was obtained when a new modified formulation of the Henry rewetting correlation was used to account for the mass rate dependence.

Hassan, Y. A., and T. K. Blanchat, 1988, "A Comparison Study of the Westinghouse Model E Steam Generator Using RELAP5/MOD2 and RETRAN-02 Computer Codes," *Third International Topical Meeting on Nuclear Power Plant Thermal Hydraulics and Operations, Seoul, Korea, November 1988.*

Comparisons of the predictions of RELAP5/MOD2 and RETRAN-02 were performed on a model of the Westinghouse Model E steam generator. This is a U-tube steam generator



with an integral preheater section. The model used was the result of a detailed nodalization study performed with the RETRAN code to determine the minimum number of nodes (or control volumes) required in the secondary side to model the response of steam generator water level and primary side exit (cold-leg) temperature during startup testing and operational transients.

A parametric study of the separator component was performed. The separator void fraction control parameters VOVER and VUNDER were varied and the effects on the steam generator circulation ratio and steam quality were investigated. It was determined that the desired circulation ratio was easily achieved but that the separator steam outlet's vapor void fraction (and corresponding steam quality) was relatively insensitive to its control parameter (VOVER). An additional parametric study was performed to study the effects of steam line exit pressure on steam quality.

Five transients were used as forcing functions to generate the response of the steam generator. The selection of these transients was based on providing both nominal and severe forcing functions on the heat removal capability of the secondary side. The steam generator transients investigated were (a) loss of feedwater, (b) turbine trip, (c) decrease in load demand, (d) increase in load demand, and (e) decrease in inlet feedwater temperature. Steam line exit mass flow rate, secondary side liquid mass inventory and water level, and primary side cold leg temperature predictions were compared with the RETRAN-02 code results. Reasonable comparisons were obtained with the RETRAN code and with qualitative behavior of simulation experiments.

Hassan, Y. A., and G. C. Henson, 1987, "RELAP5/MOD2 Simulation of GRNL Reflood Tests," *Transactions of the American Nuclear Society*, 55, pp. 454-456.

Following the blowdown phase of a postulated loss-of-coolant accident in a pressurized water reactor, the reactor core is uncovered and the fuel rods experience rapid temperature excursions because of decay power production and low heat transfer. To prevent fuel from overheating, emergency core cooling is activated and the accident enters the reflood phase. Several experimental and analytical programs have been performed to investigate the reflooding phenomena. The purpose of this study is to simulate several reflooding tests performed at Oak Ridge National Laboratory in the Thermal Hydraulic Test Facility using RELAP5/MOD2/36.04 to assess its capabilities in predicting the reflood phenomena. The code has demonstrated the capability to predict experimental behavior; however, refinements in the interfacial drag are required to improve the code's predictions.

Hassan, Y. A., and C. D. Morgan, 1986, "Comparison of Lehigh 3 x 3 Rod Bundle Post-CHF Data With the Predictions of RELAP5/MOD2," *American Nuclear Society and Atomic Industrial Forum Joint Meeting, Washington, D. C., November 1986*.

To date, there are only very limited data for nonequilibrium convective film boiling in rod bundle geometries. A recent nine (3x3)-rod bundle post-critical heat flux (CHF) from the Lehigh University test facility was simulated using RELAP5/MOD2/36.02. The simulation assessed the code's capabilities in predicting the overall convective mechanisms in post-CHF heat transfer in rod bundle geometries. The code calculations were compared with the

experimental data. With the exception of a premature quench, the cladding temperatures were in a reasonable agreement with the data. However, the code predicted low vapor superheats and void fraction oscillations.

Holmstrom, H., 1987, "Finnish Assessment of RELAP5/MOD2," *14th Water Reactor Safety Information Meeting, Gaithersburg, Maryland, October 27, 1986*, NUREG/CP-0082, Volume 5, February, pp. 133-142, Technical Research Center of Finland.

The first frozen version of RELAP5/MOD2/36 was received in Finland in February 1985. Four assessment cases and several hypothetical large pressurized water reactor cases have been calculated so far. The code has generally produced better results and run better than MOD1. However, some problems have been encountered. There still seems to be discontinuities in the code and the interphase friction seems to be excessive.

Holmstrom, H., 1986, "Technical Research Centre of Finland Use of RELAP5/MOD2," *13th Water Reactor Safety Information Meeting, Washington, D. C., October 1985*, NUREG/CP-0072, Volume 5, February, Technical Research Centre of Finland.

Reactor safety research in Finland is described in a general way, and the Technical Research Centre's computer code system for thermal hydraulic accident analysis is introduced. The role of RELAP5/MOD2 together with the current experiences and plans for future use are also discussed. According to the plans RELAP5/MOD2 will be the main tool in the analyses of large and small break loss-of-coolant accidents and some other transients together with self-developed faster computer codes. The limited experiences with RELAP5/MOD2 have been promising, although not completely without problems.

Hornig, T. S., Y. D. Huang, L. Y. Liao, C. H. Lee, and Y. B. Chen, 1988, "Assessment of RELAP5/MOD2 Using Low Pressure Two Phase Flow Distribution Data," *Third International Topical Meeting on Nuclear Power Plant Thermal Hydraulics and Operations, Seoul, Korea, November 1988*, Institute of Nuclear Energy Research.

RELAP5/MOD2 has been widely used to simulate the loss-of-accidents of light water reactors. During the blowdown, the system depressurizes from initial high pressure to near atmospheric pressure at the end of the accident. However, the general capability of RELAP5/MOD2 at near atmospheric pressure has not been extensively reviewed. A simple test facility, which contains two vertical tubes in parallel to represent the reactor coolant channels, has been established at the Institute of Nuclear Energy Research to assess the ability of RELAP5/MOD2 to predict low-pressure two-phase flow distribution.

The experimental data are compared with the computational results. In the present study, calculations with the recommended nonequilibrium option of RELAP5/MOD2 are not able to obtain realistic results because of computation failure. Although the simulated system can avoid the unphysical transient and reach steady state for all test conditions by using the thermal equilibrium option, studies have been performed to identify the causes of failure. It has been found that simulations with the nonequilibrium option and stricter mass error acceptance criteria can suppress the unrealistic oscillations and reach steady state for all tests. But only little improvement can be achieved for the differences of major hydraulics

properties between computational results and measured values. Further studies about RELAP5/MOD2 models under low-pressure conditions are suggested.

Jacobs, G., 1988, "RELAP5/MOD2 Post-Test Analysis of a Forced Feed Reflood Experiment in an Electrically Heated 61-Rod Bundle with a Tight Lattice," June, KFK-4450, *Safety-Oriented LWR Research. Annual Report 1987*, Kernforschungszentrum Karlsruhe G.m.b.H., Federal Republic of Germany, Inst. fuer Neutronenphysik und Reaktortechnik.

To test the applicability RELAP5/MOD2 to tight fuel rod lattices of advanced pressurized water reactors (PWRs) presently being investigated, a posttest analysis was performed of an experiment of the FLORESTAN-Programme. RELAP5/MOD2 was unable to adequately simulate the reflood behavior observed in the experiment. Modeling effort is needed to extend the capability of RELAP5 toward applications to advanced PWRs, especially for the reflood phase of loss-of-coolant accidents.

Jacobs, G., and A. Galvan, 1987, *Application of the Flooding Option of the RELAP5/MOD2 LWR Thermohydraulic Code to a SEFLEX Experiment, Nuclear Safety Project Annual Report, 1986*, Kernforschungszentrum Karlsruhe G.m.b.H., Federal Republic of Germany.

Using RELAP5/2/36.04, which has been installed on a CRAY X-MP at KFA Juelich via network telecommunication, posttest analyses of forced reflood tests of the SEFLEX and FLORESTAN experimental programs have been performed. A consolidated KFK-version of COMMIX-2 has been transmitted to Argonne National Laboratory. It contains most options of COMMIX-1B (excluding the skew-upwind technique) as well as new routines for the linewise, planewise, or regionwise integration of the Poisson-type pressure and enthalpy equation. Main progress in the vectorization of COMMIX-2 was the implementation of red/black-successive-over-relaxation (SOR)-algorithms for the solution of the Poisson-type equations.

Jacobson, J. L., and R. G. Hanson, 1987, "Status of the RELAP5 User Guidelines," *15th Water Reactor Safety Information Meeting, Gaithersburg, Maryland, October 26, 1987*.

This paper presents an overview of a RELAP5 user guidelines document that is currently being developed under the sponsorship of the U.S. Nuclear Regulatory Commission at the Idaho National Engineering Laboratory. The RELAP5 user guidelines will provide insight for proper code use for specific applications, and specific guidance relative to nodalization of nuclear power plants and experimental facilities based on a standard nodalization philosophy.

Johnsen, G. W., 1985, "RELAP5/MOD2 Development," *13th Water Reactor Safety Research Information Meeting, Washington, D.C., October 1985*.

RELAP5/MOD2 is a pressurized water reactor system transient analysis computer code developed for the U.S. Nuclear Regulatory Commission Safety Research and Regulatory Programs. MOD2 was officially released in April 1984. Since that time, development work has focused on refinements designed to increase code speed, usability, and reliability. Plans for FY 1986 call for continued maintenance and use support for RELAP5. In addition, a

new self-initialization option will be added to reduce the time and cost presently needed to initialize large plant models. This option will use the existing steady-state and nearly-implicit solution scheme features, coupled with a generic, built-in controller package. The latter will permit the user to specify any one of the several parameters set to be kept fixed, while other variables may "float." The steady-state option and a new solution scheme will cause the model to relax to a steady-state condition many times faster than would be physically possible.

Johansen, G. W., and Y. S. Chen, 1988, "RELAP5: Applications to High Fidelity Simulation," *Eastern Simulation Conference, Orlando, Florida*.

RELAP5 is a pressurized water reactor system transient simulation code for use in nuclear power plant safety analysis. MOD2 may be used to simulate a wide variety of abnormal events, including loss-of-coolant accidents, operational transients, and transients in which the entire secondary system must be modeled. In this paper, a basic overview of the code is given, its assessment and application illustrated, and progress toward its use as a high fidelity simulator described.

Kalyanasundaram, M., and Y. A. Hassan, 1988, "Analysis of Loss-of-Feedwater Transients in MB-2 using RELAP5/MOD2," *Transactions of the American Nuclear Society, Joint Meeting of the European Nuclear Society and American Nuclear Society, Washington, D.C., 1988, Volume 57, pp. 143-147.*

The steam generator is the major controlling component in a wide range of transients and accidents in pressurized water reactors. The need to understand the steam generator response to transient conditions has led to many experimental and analytical investigations. In this study, a RELAP5/MOD2 model was developed for the Westinghouse Model F steam generator test facility Model Boiler No. 2 (MB-2). Model Boiler No. 2 is a power scaled representation approximately equal to 0.8% of the Model F steam generator unit. The objective of the MB-2 test program was to provide comprehensive data on the thermal hydraulic behavior of the steam generator under transient conditions. The objective of this study was to simulate the test facility using Texas A&M University's RELAP5/MOD2. The code's steady-state and loss-of-feedwater transient predictions were compared with the test data. A favorable agreement was obtained. Further refinement in the heat transfer correlations in the tube bundle is needed.

Kang, J. C., B. S. Pei, G. P. Yu, and R. Y. Yuann, 1987, "Analysis of the Mannshan Unit 2 Full Load Rejection Transient," *Transactions of the American Nuclear Society, 55, pp. 468-470, November, National Tsing-Hua University, Taiwan.*

Mannshan Unit 2 is a Westinghouse three-loop pressurized water reactor with a rated core power of 2775 MW (thermal) and a rated core flow of 4702 kg/s. Before full power operation, a planned net load rejection was performed during the startup test by opening the main transformer highside breakers. The generator power rapidly reduced to station load. All 16 steam dump valves immediately popped open, and control bank-D rods automatically stepped in as the temperature difference  $T_{\text{sub avg}} - T_{\text{sub ref}}$  reached a programmed 2.8°C. Nuclear power decreased smoothly as control rods were inserted into

the core. The pressurizer pressure and liquid levels also dropped. Neither safety injection nor reactor trip occurred during this transient. The test was done to verify that the whole system would function properly under a transient to keep the reactor from scrambling and that the vessel integrity would also be protected. In this study, which is the preliminary stage of RELAP5/MOD2 transient simulation of the Mannschan pressurized water reactor plants, system thermal-hydraulic response is tested first and isolated from the neutronic effects. The variation of core power versus time curve was extracted from the power test data to serve as a time varying boundary condition. The comparison of the analytical results of four major parameters (pressurizer pressure, average temperature of the core, steam dump flow rate, and feedwater flow rate) from RELAP5/MOD2 and the power test data are illustrated. The analytical results agreed reasonably well with the measured data in trend and magnitude. The pressurizer pressure is the most deviant parameter, being lower than the power test data throughout the transient.

Kim, S. S., and J. C. McKibben, 1989, "PARET/ANL and RELAP5/MOD2 Benchmarking Comparison with the SPERT-IV Test Data," *Annual Meeting of the American Nuclear Society, Atlanta, Georgia, June 1989*.

Results of the PARET/ANL and RELAP5/MOD2 computations on one of the SPERT-IV tests are compared to select the code that best predicts the peak power and fuel plate temperature resulting from reactivity-induced transients for use in the University of Missouri Research Reactor (MURR) upgrade safety-related analysis. The D-12/25 core of the SPERT-IV tests was selected for comparison because the test was performed under forced coolant circulation in a low-pressure and low-temperature environment, and this test used plate-type fuel (like MURR). The square-shaped D-12/25 core consisted of a 5x5 array of 20 fuel assemblies, 4 control rod assemblies, and 1 transient rod assembly. Control of the reactor was accomplished by the use of four boron/aluminum control rods, and the power excursion was initiated by a step reactivity addition established by ejecting the poison section of the transient rod from the core.

Klingenfus, J. A., and M. V. Parece, 1989, *Multiloop Integral System Test (MIST) Final Report: RELAP5/MOD2 MIST Analysis Comparisons*, B&W-2078-VOL-10, EPRI-NP-6480-VOL-10, December.

The Multiloop Integral System Test (MIST) Facility is part of a multiphase program started in 1983 to address small break loss-of-coolant accidents (SBLOCAs) specific to Babcock & Wilcox (B&W) designed plants. MIST is sponsored by the U.S. Nuclear Regulatory Commission, the B&W Owners Group, the Electric Power Research Institute and B&W. The unique features of the B&W design, specifically the hot leg U-bends and steam generators, prevented the use of existing integral system data or existing integral system facilities to address the thermal-hydraulic SBLOCA questions. MIST and two other supporting facilities were specifically designed and constructed for this program, and an existing facility, the Once-Through Integral System, was also used. Data from MIST and the other facilities will be used to benchmark the adequacy of system codes, such as RELAP5/MOD2 and TRAC-PF1, for predicting abnormal plant transients. The MIST Program included funding for seven individual RELAP pretest and posttest predictions.



The comparisons against data and final conclusions are the subject of this volume of the MIST Final Report.

Kolar, W., H. Staedtke, and B. Worth, 1987, "JRC ISPRA Experience with IBM Version of RELAP5/MOD2," *14th Water Reactor Safety Information Meeting, Gaithersburg, Maryland, October 27, 1986*, NUREG/CP-0082, Volume 5, pp. 305-328, February. Commission of the European Communities, Ispra, Italy.

Various RELAP5 code versions have been used extensively within the LOBI Project at the Joint Research Center in Ispra, Italy for test design calculations, pretest predictions, and posttest analysis. The results obtained represent an important contribution to the multi-national effort for the RELAP5 code assessment. The paper focuses mainly on RELAP5/MOD2/36.04. Problems related to the conversion of the code from Control Data Corporation (CDC) to an IBM compatible form are outlined in the paper. The prediction capability of the code is demonstrated by comparison of predicted and measured data for different LOBI integral system experiments.

Laats, E. T., 1987, "Nuclear Plant Analyzer Development at the Idaho National Engineering Laboratory," *14th Water Reactor Safety Information Meeting, Gaithersburg, Maryland, October 27, 1986*, NUREG/CP-0082, Volume 5, pp. 41-44, February.

The Nuclear Plant Analyzer (NPA) is a state-of-the-art safety analysis and engineering tool being used to address key nuclear power plant safety issues. Under the sponsorship of the U.S. Nuclear Regulatory Commission (NRC), the NPA has been developed to integrate the NRC's computerized reactor behavior simulation codes such as RELAP5, TRAC-BWR and TRAC-PWR, with well-developed computer color graphics programs and large repositories of reactor design and experimental data. An important feature of the NPA is the capability to allow an analyst to redirect a RELAP5 or TRAC calculation as it progresses through its simulated scenario. The analyst can have the same power plant control capabilities as the operator of an actual plant. The NPA resides on the dual Control Data Corporation Cyber 176 mainframe computers at the Idaho National Engineering Laboratory (INEL) and Cray-1S computers at Los Alamos National Laboratory (LANL) and Kirtland Air Force Weapons Laboratory (KAFWL). During the past year, the NPA program at the INEL has addressed two primary areas: software development and user support. These activities are discussed in the paper.

Laats, E. T., 1987, "USNRC's Nuclear Plant Analyzer: Engineering Simulation Capabilities into the 1990's," *International Nuclear Simulation Symposium and Mathematical Modeling Workshop*, Schliersee, Federal Republic of Germany, October 13, 1987.

The Nuclear Plant Analyzer (NPA) is the U.S. Nuclear Regulatory Commission's (NRC's) state-of-the-art nuclear reactor simulation capability. This computer software package integrates high fidelity nuclear reactor simulation codes such as the TRAC and RELAP5 series of codes with color graphics display techniques and advanced workstation hardware. The NPA first became operational at the Idaho National Engineering Laboratory in 1983. Since then, the NPA system has been used for a number of key reactor safety-related tasks ranging from plant operator guidelines evaluation to emergency preparedness training. The

NPA system is seen by the NRC as their vehicle to maintain modern, state-of-the-art simulation capabilities for use into the 1990's. System advancements are envisioned in two areas: (a) software improvements to existing and evolving plant simulation codes used by the NPA through the use of such techniques as parallel and vector processing and artificial intelligence expert systems, and (b) advanced hardware implementations using combinations of super-, minisuper-, supermini-, and supermicrocomputer system and satellite data communications networks for high flexibility and greatly increased NPA system performance.

Laats, E. T., 1984, "Nuclear Plant Analyzer Development and Analysis Applications," *International Thermal Hydraulic and Plant Operations Topical Meeting, Taipei Taiwan, October 1984*.

The Nuclear Plant Analyzer (NPA) is being developed as the U.S. Nuclear Regulatory Commission's (NRC's) state-of-the-art safety analysis and engineering tool to address key nuclear plant safety issues. The NPA integrates the NRC's computerized reactor behavior simulation codes such as RELAP5 and TRAC-BWR, both of which are well-developed computer graphics programs and large repositories of reactor design and experimental data. Using the complex reactor behavior codes and the experiment data repositories enables simulation applications of the NPA that are generally not possible with more simplistic, less mechanistic reactor behavior codes. These latter codes are used in training simulators or with other NPA-type software packages and are limited to displaying calculated data only. This paper describes four applications of the NPA in assisting reactor safety analyses. Two analyses evaluated reactor operating procedures during off-normal operation for a pressurized water reactor and a boiling water reactor, respectively. The third analysis was performed in support of a reactor safety experiment conducted in the Semiscale facility. The final application demonstrated the usefulness of atmospheric dispersion computer codes for site emergency planning purposes. An overview of the NPA and how it supported these analyses are the topics of this paper.

Laats, E. T., et. al., 1985, "Nuclear Plant Analyzer Development at the Idaho National Engineering Laboratory," *13th Water Reactor Safety Research Information Meeting, Washington, D.C., October 1985*.

The Nuclear Plant Analyzer (NPA) is a state-of-the-art safety analysis and engineering tool being used to address key nuclear power plant safety issues. Under the sponsorship of the U.S. Nuclear Regulatory Commission (NRC), the NPA has been developed to integrate the NRC's computerized reactor behavior simulation codes, such as RELAP5, TRAC-BWR, and TRAC-PWR, with well-developed computer color graphics programs and large repositories of reactor design and experimental data. An important feature of the NPA is the capability to allow an analyst to redirect a RELAP5 or TRAC calculation as it progresses through its simulated scenario. The analyst can have the same power plant control capabilities as the operator of an actual plant. The NPA resides on the dual Control Data Corporation Cyber-176 mainframe computers at the Idaho National Engineering Laboratory and a CRAY-1S computer at Los Alamos National Laboratory.

Laats, E. T., and R. N. Hagen, 1985, "Nuclear Power Plant Simulation Using Advanced Simulation Codes through a State-of-the-Art Workstation," *Proceedings of the 1985 Summer Computer Simulation Conference, Chicago, Illinois, July*, pp. 397-401.

The Nuclear Plant Analyzer (NPA) currently resides in a Control Data Corporation 176 mainframe computer at the Idaho National Engineering Laboratory (INEL). The NPA user community is expanding to include worldwide users who cannot consistently access the INEL mainframe computer from their own facilities. Thus, an alternate mechanism is needed to enable their use of the NPA. Therefore, a feasibility study was undertaken by EG&G Idaho, Inc. to evaluate the possibility of developing a stand-alone workstation dedicated to the NPA. The basic requirements for the workstation are the ability to (a) run the RELAP5 and TRAC-BWR nuclear reactor simulation codes (which are part of the NPA) at real wall-clock time computational speeds, (b) integrate all other NPA color graphics and data base functions, (c) assemble the necessary workstation hardware using off-the-shelf components at a total price of less than \$250,000, and (d) develop the entire system in five years. A workstation of this type with these simulation codes has only been possible to date on a Class VI mainframe computer (e.g., CRAY.XMP).

Larson, T. K., and R.A. Dimenna, 1987, "Preservation of Natural Circulation Similarity Criteria in Mathematical Models," *24th National Heat Transfer Conference and Exhibition, Pittsburgh, Pennsylvania, August 9, 1987*.

This paper discusses preservation of similitude criteria in current mathematical models used for transient analysis of thermal-hydraulic systems. Input models for the RELAP5 computer code were developed at the Idaho National Engineering Laboratory for two simple hypothetical natural circulation systems consisting of a closed loop containing energy generation, energy removal, and flow resistance. The two models differ significantly in geometric scale size. A reference model had components and operating conditions in a range similar to those found in typical nuclear steam supply systems, a scaled model, geometrically much smaller than the reference model, had components that were sized from the reference model using similarity criteria presented in the literature. Steady-state and transient single- and two-phase natural circulation calculations were conducted using both models to determine if the model-to-model relationships in time, pressure drop, and velocity scales were in accordance with the similitude criteria. Results indicate that while the code predicts the expected fundamental effects of geometric scale, there are noteworthy differences in the details of calculations.

Lee, Y. J., B. D. Chung, and H. J. Kim, 1988, "Analysis of Kori 1 Station Blackout Accident for RELAP5/MOD2 Assessment," *Third International Topical Meeting on Nuclear Power Plant Thermal Hydraulics and Operations, Seoul, Korea, November 1988*, Korea Advanced Energy Research Institute.

The station blackout accident at 77.5% power that occurred on June 9, 1981 at the Kori Unit 1 pressurized water reactor (PWR) is simulated using the RELAP5/MOD2 system thermal hydraulic computer code. Major thermal hydraulic parameters are compared with the available plant data. The establishment of the natural circulation following the trips of both coolant pumps is confirmed. The calculated reactor coolant flow rate closely

approximates the plant data validating the relevant thermal hydraulic models of RELAP5/MOD2. Results also show that the supply of auxiliary feedwater without the operation of the steam generator power-operated relief valves (S/G PORVs) is sufficient for removing the decay heat of the core.

A postulated station blackout accident with the similar sequence of events as the one described above is analyzed. The results confirm that the safety of Kori 1 is secured by the actuation of S/G PORVs coupled with the supply of auxiliary feedwater. The comparison of the analysis results with the plant data demonstrates that the RELAP5/MOD2 code has the capability to simulate the thermal hydraulic behavior of PWRs under accident conditions of this type with accuracy. It is also recognized that for best-estimate based transient analyses, the characteristics of such non-safety related components as the turbine stop valve closing time, and S/G PORV setpoints have significant impact on the results; thus, the accuracy with which they are simulated is important.

Liang, K. S., L. Kao, L. Y. Liao, and Y. B. Chen, 1988, "Best Estimate Analysis of Recirculation Pump Suction Like Small-Break LOCA of Kuosheng BWR/6 Nuclear Power Plant," *Third International Topical Meeting on Nuclear Power Plant Thermal Hydraulics and Operations, Seoul, Korea, November 1988*, Institute of Nuclear Energy Research, Taiwan.

A simulation model of the Kuosheng BWR/6 Power Plant is developed using the RELAP5/MOD2 code to investigate the system thermal response and define necessary operator actions during a recirculation suction line small break (0.2 ft<sup>2</sup>) loss-of-coolant accident (LOCA) with or without the assumption of safety system failures. The calculation results show that even with the safety system failures assumed, the plant can successfully withstand the small break LOCA. The high-pressure systems must fail to cause a partial core heatup. The results also show that the function of the automated depressurization system plays an important role in mitigation of the consequences of the small break LOCA.

Liang, K. S., L. Kao, L. Y. Liao, and Y. B. Chen, 1988, "Assessment of the RELAP5/MOD2 Code Using MSIV Fast Closure Test Data of Kuosheng BWR-6 Nuclear Power Plant," *Third International Topical Meeting on Nuclear Power Plant Thermal Hydraulics and Operations, Seoul, Korea, November, 1988*, Institute of Nuclear Energy Research, Taiwan.

The water level tracing capability of computer codes is important for light water reactor simulation [especially for boiling water reactors (BWRs)] to estimate water inventory remaining during either transitory or accidental conditions. RELAP5/MOD2 has been extensively applied in pressurized water reactors, but less frequently applied to BWRs. In this paper, a set of plant test data of the Taipower's Kuosheng Nuclear Power Plant, a BWR-6 Mark-III containment plant, is used to assess the BWR modeling capability of RELAP5/MOD2, particularly for water level prediction. Because the main station isolation valve (MSIV) fast closure event occasionally occurred during operation and because it will cause water levels to change heavily, the test of MSIV fast closure is adopted. Through comparisons, it was observed that results produced by RELAP5 simulation are in good agreement with the test data.



Lin, J. C., R. A. Riemke, V. H. Ransom, and G. W. Johnsen, 1984, "RELAP5/MOD2 Pressurizer Modeling," *ASME Winter Meeting, New Orleans, Louisiana December 1984*.

The objective of this paper is to present the RELAP5/MOD2 models for describing repressurization transients and to report the developmental assessment results obtained through simulation of several separate effects experiments. RELAP5/MOD2 contains improved modeling features that provide a generic pressurized water reactor transient simulation capability. In particular, the nonequilibrium capability has been generalized to include repressurization transients in which subcooled liquid and superheated vapor may coexist in the pressurizer and/or other locations in the primary coolant system. The assessment shows that RELAP5/MOD2 calculated results are in good agreement with data and the nonequilibrium phenomena for repressurization transients are properly modeled.

Loomis, G. G., and J. E. Streit, 1985, *Results of Semiscale MOD-2C Small-Break (5%) Loss-of-Coolant Accident Experiment S-LH-1 and S-LH-2*, NUREG/CR-4438, EGG-2424, November.

Two experiments simulating small break (5%) loss-of-coolant accidents (5% SBLOCAs) were performed in the Semiscale MOD-2C facility. These experiments were identical except for downcomer-to-upper-head bypass flow (0.9% in Experiment S-LH-1 and 3.0% in Experiment S-LH-2) and were performed at high pressure and temperature [15.6 MPa (2262 psia)-system pressure, 37K (67°F)-core differential temperature, 595K (610°F)-hot leg fluid temperature]. From the experimental results, the signature response and transient mass distribution are determined for a 5% SBLOCA. The core thermal hydraulic response is characterized, including core void distribution maps, and the effect of core bypass flow on transient severity is assessed. Comparisons are made between postexperiment RELAP5 calculations and the experimental results, and the capability of RELAP5 to calculate the phenomena is assessed.

Loomis, G. G., and J. E. Streit, 1985, *Quick Look Report for Semiscale MOD-2C Experiments S-LH-1 and S-LH-2*, EGG-SEMI-6884, May.

Results from a preliminary analysis of Semiscale Tests S-LH-1 and S-LH-2 are presented. Both experiments were 5%, cold leg, centerline pipe break, loss-of-coolant accident simulations the only difference was the downcomer to upper head bypass flow. Phenomena of interest included two core liquid level depressions with minor core rod temperature excursions. The first liquid level depression was induced by a manometric balance formed by a liquid seal in the pump suction of both loops, and the second level depression was due to core liquid boiloff. Pump suction seal clearing mitigated the first core heatup. Comparisons are made between a pretest RELAP5 calculation and S-LH-1 data. RELAP5 calculated the manometric core level depression but not the core rod heatups.

Loomis, G. G., T. K. Larson, and J. E. Streit, 1987, "Natural Circulation Cooling During a Small-Break Loss-of-Coolant Accident in a Simulated Pressurized Water Reactor," *ASME International Symposium on Natural Circulation, Boston, Massachusetts, December 17, 1987*.



The paper presents experiment results from a simulated small break loss-of-coolant accident (SBLOCA) involving natural circulation core heat rejection mechanisms. The experiment results are compared to pre-experiment RELAP5/MOD2 calculations, and are related to expected pressurized water reactor (PWR) behavior during SBLOCA conditions. The simulation conducted in the Semiscale MOD-2C scaled-experiment facility was a 0.5% cold leg centerline break performed at high temperature and pressure with initial conditions typical of a PWR (15.6-MPa pressure, 587-K hot leg fluid temperature). The Semiscale MOD-2C facility represents all major components of a large PWR; the facility includes active loops, steam generators, and a vessel with an electrically heated core. The transition from forced circulation to the various modes of natural circulation was characterized in the Semiscale simulation. The natural circulation cooling modes observed include single-phase, two-phase, and reflux. Analysis included extensive decoupling of natural circulation heat rejection modes between the loops, and multi-dimensional effects within the steam generator U-tube. A comparison of RELAP5/MOD2 calculation with the data shows correct qualitative calculations of the occurrence of single-phase, two-phase, and reflux cooling during the Semiscale transient. Analysis of similitude criteria for the Semiscale facility suggests that the Semiscale results preserve the first-order effects thought important for natural circulation phenomena expected in a PWR.

Lucas, S., T. Hudson, and M. Pope, 1987, "Comparison of a RELAP5/MOD2 Thermal-Hydraulic Model to Plant Data for a Turbine Trip Test," *Transactions of the American Nuclear Society*, 55, pp. 697-698

Shearon Harris Unit One is a three-loop Westinghouse 2775-MW (thermal) nuclear power plant owned and operated by Carolina Power & Light Company. A RELAP5/MOD2/36.04 thermal hydraulic model of Unit One has been constructed to support operations and probabilistic risk analysis. The three-loop model used in this study has 162 volumes and 175 junctions. At the present time, the model has control systems for the steam dump system, pressurizer level control, steam generator level, secondary mass inventory, primary average temperature, and various trips. To validate the model, the turbine trip startup test was chosen for the benchmark comparison. The model was initialized at 97% thermal power, since this was the power at which the turbine trip test was performed. The results of the comparisons from the test indicate that the model does reasonably well in reproducing plant response. Additional plant parameters such as pressurizer level, steam generator level, and steam line pressure also compare favorably to plant data. Immediate plans include using the model for probabilistic risk assessment success criteria and incorporating additional controllers and trips. Additional comparison to plant data will also be performed.

Makowitz, H., and W. H. Gray, 1987, "Investigation of Time-Step Insensitivity for RELAP5/MOD2 SBLOCA Simulations," *Transactions of the American Nuclear Society*, 55, pp. 363-364.

Time step insensitivity, accuracy, and temporal convergence have been demonstrated for a small break loss-of-coolant accident (SBLOCA) simulation using the production version of RELAP5/MOD2 for a maximum time step  $\Delta t_{max}$  of 0.01 less than or equal to  $\Delta t_{max}$  less than or equal to 0.125 s for a 200-s calculation. An improved, generalized,

underrelaxation scheme has been developed where the underrelaxation parameter is only a function of the Courant number,  $N_c$ . This new underrelaxation scheme allows the RELAP5/MOD2 code to execute using larger time steps, limited only by the material Courant limit and mass error considerations. Temporal convergence, accuracy, and time-step insensitivity for this new scheme have been demonstrated using maximum time step values,  $\Delta t_{max}$ , of 0.01, 0.125, and 2.0 s for 200 s of the SBLOCA problem simulations. The authors plan to extend this study to 1000-s simulations and to investigate round-off error propagation associated with performing RELAP5 SBLOCA calculations on computers of different word sizes. They also plan to accommodate flow reversal and extend the new underrelaxation scheme to the region where  $\Delta t$  is less than or equal to 0.05 s.

Makowitz, H., and R. J. Wagner, 1987, "Progress with Algorithm and Vector/Parallel Enhancements for RELAP5/MOD2 Thermohydraulic System Simulation Code," *International Topical Meeting on Advances in Reactor Physics, Mathematics and Computation, Paris, France, April 27-30, 1987*.

Earlier experience resulting from attempts to develop a parallel implementation and a vector implementation for RELAP5/MOD1 using super computers resulted in an analysis suggesting a five to ten times performance enhancement for future versions of the code. The MOD2 version of the code, presently available, uses a six equation model (vs. five equations in MOD1) with the option of a semi-implicit or nearly-implicit numerical solution scheme. The nearly-implicit numerical scheme violates the convective (material) Courant limit. The RELAP5/MOD2 code has been implemented on Control Data Corporation Cyber 176, CRAY 1S, and CRAY X-MP/48 computers. Algorithm performance enhancements and vector performance improvements have been measured and are analyzed for these three computing machines. The reactor small break loss-of-coolant problem used in previous studies was employed as the basis for the present analysis. Previous studies performed to compare the performance of algorithms in MOD2 are compared to MOD1, using the two presently available numerical methods in MOD2. Planned vector and parallel enhancements are discussed in the context of past studies and expected future performance gains. Applicability of the RELAP5 code to best-estimate real time simulations and nuclear power plant simulators is discussed.

McCreery, G. E., K. G. Condie, and M. P. Plessinger, 1988, "B&W Once-Through Steam Generator Single Tube Experiment Results," *15th Water Reactor Safety Information Meeting, Gaithersburg, Maryland, October 26, 1987*.

Experiments are being conducted in an air-water facility that models Babcock & Wilcox once-through steam generator (OTSG) heat transfer and fluid flow behavior during auxiliary feedwater (AFW) injection. The OTSG is a single-pass counterflow tube-in-shell heat exchanger. Decay heat is removed by injecting AFW into the steam generator boiler region. AFW is injected near the top of the bundle, typically through seven penetrating nozzles at the periphery of the bundle, and results in a complex steam-water counterflow situation within the boiler. As AFW is injected, it tends to fall downward because of gravity and inward because of momentum. Fluid flow is impeded and redistributed by tube support plates (TSPs) spaced along the bundle and by steam flow up the bundle. The single tube experiments described in this paper are the first in a series that examines the

basic phenomena of AFW radial and axial flow distribution, TSP flooding, and tube heat transfer. The succeeding experiments, which are presently underway, address the AFW behavior in an unheated multi-tube (625 tubes) full-scale 1/8 sector of the OTSG that includes the top three TSPs. The overall objective of the experiment series is to obtain observations and data of steam generator fluid flow and heat transfer phenomena to develop improved RELAP5 and TRAC code models. This paper describes data obtained in the single tube experiments conducted to date. The relevant phenomena observed are described and the data are analyzed. The analysis is preliminary for the heat transfer data since it employs a computer program that is presently under development.

Megahed, M. M., 1987, *RELAP5/MOD2 Assessment Simulation of Semiscale MOD-2C Test S-NH-3*, NUREG/CR-4799, EGG-2519, June.

This report documents an evaluation of the RELAP5/MOD2/36.05 thermal hydraulic computer code for a simulation of a small break loss-of-coolant accident (SBLOCA) transient. The experimental database for the evaluation is the results of Test S-NH-3 performed in the Semiscale MOD-2C test facility. The test modeled a 0.5% SBLOCA with an accompanying failure of the high-pressure injection emergency core cooling system. The test facility and RELAP5/MOD2 model used in the calculations are described. Evaluations of the accuracy of the calculations are presented in the form of comparisons of measured and calculated histories of selected parameters associated with the primary and secondary systems. The conclusion was that the code is capable of making SBLOCA calculations efficiently. However, some of the SBLOCA-related phenomena were not properly predicted by the code, suggesting a need for code improvement.

Miettinen, J., T. Kervinen, H. Tuomisto, and H. Kantee, 1987, "Oscillations of Single-Phase Natural Circulation During Overcooling Transients," *American Nuclear Society Anticipated and Abnormal Transients in Nuclear Power Plants, Atlanta, Georgia, April*.

Strong oscillations of single-phase natural circulation were found when analyzing overcooling transients of Loviisa Unit 1 reactor pressure vessel with the system codes RELAP5/MOD2 and SMABRE. SMABRE is a fast-running code for small break loss-of-coolant accident analyses. The low flow rate periods of an oscillating natural circulation may cause significant temperature decrease in the cold leg and downcomer when the high-pressure safety injection is used. Therefore, oscillation phenomena need to be studied further to define their importance for reactor vessel integrity. Similar oscillations have been found in RELAP5 calculations of the H. B. Robinson Unit 2 steam generator tube rupture sequence in connection with the integrated pressurized thermal shock study. The oscillations were explained qualitatively to result from the one-dimensional node model. The purpose of this paper is to demonstrate that observed single-phase natural circulation oscillations can occur in a one-dimensional representation. Qualitative judgments and system calculations are used to show that these oscillations will be strongly damped in a three-dimensional geometry.

Miller, C. S., 1986, "RELAP5/MOD2 Development," *14th Water Reactor Safety Information Meeting, Gaithersburg, Maryland, October 27.*

RELAP5/MOD2 is a pressurized water reactor system transient analysis computer code developed for the U.S. Nuclear Regulatory Commission Safety Research and Regulatory Programs. MOD2 was officially released in April 1984. Since that time, development has focused on refinements designed to increase code speed, usability, and reliability.

Mirkovic, D., and D. J. Diamond, 1990, *Boron Flushing During a BWR Anticipated Transient Without Scram*, NUREG/CR-5573, BNL-NUREG-52237, June.

This report documents a study of an accident sequence in a boiling water reactor in which there is a large reactivity insertion because of the flushing of borated water from the core. This has the potential to occur during an anticipated transient without scram after the injection of borated water from the standby liquid control system. The boron shuts down the power, but if there is a rapid depressurization of the vessel (e.g., due to the inadvertent actuation of the automatic depressurization system), large amounts of low pressure, relatively cold, unborated water enter the vessel causing a rapid dilution and cooling. This study was carried out to determine if the reactivity addition caused by this flushing could lead to a power excursion sufficient to cause catastrophic fuel damage. Calculations were carried out using the RELAP5/MOD2 computer code under different assumptions regarding timing and availability of low-pressure pumps and with different reactivity coefficients. The results showed that the fuel enthalpy rise was insufficient to cause catastrophic fuel damage, although less severe fuel damage might still be possible from the overheating of the fuel cladding.

Miro, J., H. G. Sonnenburg, F. Steinhoff, V. Teschendorff, A. Forge, R. Pochard, and A. Porrachia, 1987, *Study on the State of the Art of the Development of Some Thermal-Hydraulic Safety Codes for PWR Systems, Part One: Code Description, and Part Two: Code Comparison*, EUR-11522, Draft, March, Gesellschaft für Reaktorsicherheit.

This report is concerned with thermal hydraulic phenomena on the primary and secondary side of pressurized water reactors. It is addressed to engineers and scientists who would like to improve their knowledge of the model and the phenomena description, which is existing in the different codes. It should also be of interest for persons who need an overview on existing codes. The selected codes are ALMOD (Federal Republic of Germany), CATHARE (France), DRUFAN/FLUT (Federal Republic of Germany), RELAP5/MOD2 (US), THYDE P2 (Japan), TRAC/PF1/MOD1 (US). The report is divided into two parts. The first part presents all relevant information (e.g., structure, physical models, and numerical solution schemes) code by code with a common structure. The second part is devoted to a systematic comparison of main features, corresponding to the structure of the part 1 code description, and to quantitative comparisons concerning some important specific phenomena (e.g., interfacial friction, mass transfer) and structure to fluid heat transfer.

(OTE: This report is restricted to International Code Assessment Program members unless specific permission is granted by the authors.

Moeyaert, P., and E. Stubbe, 1989, *Assessment Study of RELAP5/MOD2, Cycle 36.04 Based on Spray Start-up Test for DOEL-4*, ICAP Number 00045, July, Brussels, Belgium.

This report presents an assessment study for RELAP5/MOD2 based on a pressurizer spray startup test of the DOEL-4 power plant. DOEL-4 is a three-loop Westinghouse pressurized water reactor plant ordered by the EBES utility with a nominal power rating of 1000 MWe and equipped with preheated Type E steam generators. The pressurizer spray and heater test (SU-PR-01), one of a large series of commissioning tests are normally performed on new plants, was performed on February 2, 1985. TRACTEBEL, being the Architect-Engineer for this plant was closely involved with all startup tests and was responsible for the final approval of the tests.

Nilsson, L., and A. Sjoeborg, 1987, *Analysis of Breaks in Pipe Connections to the Hot Leg and to the Loop Seal in the Primary System of Ringhals 2 PWR*, in Swedish, STUDEVIK-NP-87-57, May 17, Swedish Nuclear Power Inspectorate, Stockholm; Studsvik Energiteknik AB, Nykoeeping, Sweden.

Analysis has been made of seven different cases of breaks in pipes connected to the hot leg and the loop seal in the Ringhals 2 pressurized water reactor. The pipes, in which guillotine breaks are postulated, have nominal diameters ranging from 1 to 14 inches. The analysis supplements the basis for a review of the inspection procedures for the safe-ty of pressure vessels prescribed by the Swedish Nuclear Power Inspectorate. A similar analysis already exists concerning breaks in the cold leg connections. The analysis has been made using the thermal hydraulic computer code RELAP5/MOD2 and with best estimate assumptions. This means that normal operating conditions have been adopted for the input to the calculations. However, the capacity of the safety injection system was assumed to be reduced by having one pump not operating in each of the low-pressure and high-pressure safety injection systems. The results of the analysis are presented in tables and as computer plots. The analysis shows that the consequences with respect to increased fuel rod and cladding temperatures are quite harmless. Only the two cases with the largest break sizes lead to critical heat flux (CHF) and increased temperatures for the hottest rods in the core. The peak cladding temperature was 636°C for the 12-in. break. In both cases, rewetting occurred within 25 s of accident initiation. In the cases with breaks in connections of 6-in. diameter and smaller, the RELAP5 calculations indicated a substantial margin to CHF throughout the transients.

Nithianandan, C. K., 1986, "Calculation of Once-Through Steam Generator Performance Using RELAP5/MOD2," *American Nuclear Society and Atomic Industrial Forum Joint Meeting, Washington, D. C., November 1986*.

Three steam generator performance tests from the Babcock & Wilcox 19-tube, once-through steam generator (OTSG) test facility were simulated using RELAP5/MOD2/36.01, and the results were compared with the experimental data. RELAP5 predicted the steam generator steady-state performance reasonably well.



However, further refinements to the boiling and post-critical heat flux heat transfers would improve the capability to correctly predict OTSG behavior.

Nithianandan, C. K., et. al., 1985, "RELAP5/MOD2 Code Assessment," *Transactions of the American Nuclear Society*, pp. 326-327, *American Nuclear Society Winter Meeting, San Francisco, California, November 1985*, Volumes 50 and 51.

Babcock and Wilcox (B&W) has been working with the code developers at EG&G Idaho, Inc. and the U.S. Nuclear Regulatory Commission in assessing the RELAP5/MOD2 computer code for the past year by simulating selected separate-effects tests. The purpose of this assessment has been to evaluate the code for use in the Multiloop and On-Through Integral System Tests simulations and in the prediction of pressurized water reactor transients. B&W evaluated various versions of the code and made recommendations to improve code performance. As a result, the currently released version (Cycle 36.0) has been improved considerably over earlier versions. However, further refinements to some of the constitutive models may still be needed to further improve the predictive capability of RELAP5/MOD2. The following versions of the code were evaluated:

(a) RELAP5/MOD2/22 - first released version, (b) RELAP5/32 - EG&G Idaho test version of RELAP5/MOD2/32, (c) RELAP5/MOD2/36 - frozen cycle for international code assessment, (d) updates to Cycle 36 based on recommendations developed by B&W during the simulation of a Massachusetts Institute of Technology pressurizer test, and (e) Cycle 36.1 updates received from EG&G Idaho, Inc.

Nithianandan, C. K., N. H. Shah, and R. J. Schomaker, 1985, "RELAP5/MOD2 Assessment at Babcock & Wilcox," *13th Water Reactor Safety Research Information Meeting, Washington, D.C., October 1985*.

Babcock & Wilcox (B&W) has been working with the code developers at EG&G Idaho, Inc. and the U.S. Nuclear Regulatory Commission in assessing the RELAP5/MOD2 computer code for the past year by simulating selected separate effects tests. The purpose of this B&W Owners Group-sponsored assessment was to evaluate RELAP5/MOD2 for use in design calculations for the Multiloop and Once-Through Integral System Tests and in the prediction of pressurized water reactor transients. B&W evaluated various versions of the code and made recommendations to improve code performance. As a result, the currently released version (Cycle 36.01) has been improved considerably over earlier versions. However, further refinements to some of the constitutive models may still be needed to further improve the predictive capability of RELAP5/MOD2.

Nordic Liaison Committee for Atomic Energy, 1985, *Computer Codes for Small-Break Loss-of-Coolant Accidents, Final Report of the NKA project SAK-3*, September.

An assessment of computer codes for analysis of small break loss-of-coolant accidents (SBLOCAs) is performed. The work comprises the American systems codes TRAC-PF1, RELAP5/MOD1, RELAP5/MOD2, and the Finnish fast-running code SMABRE, which are assessed theoretically and by comparative calculations of five SBLOCA experiments. On this basis, comparisons are made of the advantages and drawbacks of each code to conclude

which should be selected for SBLOCA analysis. A recommendation of necessary modifications is included.

Nordic Liaison Committee for Atomic Energy, 1985, *Heat Transfer Correlations in Nuclear Reactor Safety Calculations*, RISO-M-2504, June.

Heat transfer correlations, most of them incorporated in the heat transfer packages of the nuclear reactor safety computer programs RELAP5, TRAC-PF1 and NORA, have been tested against a relevant set of transient and steady-state experiments. In addition to usually measured parameters, the calculations provided information on other physical parameters. Results are presented and discussed. The report consists of a main report (Volume I) and appendixes (Volume II). Volume I is recommended for those looking for main results rather than details; the appendixes will be useful for computer program developers.

Owca, W. A., 1986, *Quick Look Report for Semiscale MOD-2C Experiment S-NH-1*, EGG-RTH-7147, February.

Results are presented of a preliminary analysis of the first test performed in the Semiscale MOD-2C Small Break, Loss-of-Coolant Accident Without HPI (NH) series. Test S-NH-1 simulated a pressurized water reactor transient initiated by the shear of a small diameter penetration in a cold leg, equivalent to 0.5% of the cold leg flow area. The high-pressure injection system was assumed to be inoperative throughout the transient. Recovery was initiated on a high core temperature signal and consisted of latching open both steam generator atmospheric dump valves and normal accumulator operation. The test results provided a measured evaluation of the effectiveness of automatic plant responses and operator controlled recovery operations in mitigating the effects of a small break loss-of-coolant accident when high-pressure injection is unavailable. Test data were compared to RELAP5/MOD2. Data from this test will be examined to evaluate event signatures and event severities in Semiscale and recovery procedures, with the principal objective of providing data to the benchmark computer code (RELAP5) calculations. Test data will also be compared to other tests in the series to assess the effects of break size and alternative operator recovery operations.

Owca, W. A., and T. H. Chen, 1985, *Quick Look Report for Semiscale MOD-2C Test S-FS-1*, EGG-SEMI-6858, May.

Results are presented of a preliminary analysis of the second test performed in the Semiscale MOD-2C Steam Generator Feedwater and Steam Line Break (S-FS) experiment series. Test S-FS-1 simulated a pressurized water reactor transient initiated by a double-ended offset shear of a steam generator main steam line downstream of the flow restrictor. Initial conditions represented normal full-scale plant "hot-standby" operation. The transient included an initial 600-s period in which only automatic plant protection systems responded to the initiating event. This period was followed by a series of operator actions necessary to stabilize the plant. Test data were compared with the RELAP5/MOD2 computer code and provided a basis for comparison with other tests in the series of the

effects of break size and location of primary overcooling and primary-to-secondary heat transfer.

- Park, R. J., Y. Jin, S. D. Suk, and S. K. Chae, 1988, "Analysis of Station Blackout Transient for Kori Nuclear Power Plant Unit 1," *Third International Topical Meeting on Nuclear Power Plant Thermal Hydraulics and Operations, Seoul, Korea, November 1988*, Korea Advanced Energy Research Institute.

The postulated transients associated with station blackout were analyzed for the Kori Nuclear Power Plant Unit 1. The base transient, the TMLB' sequence, assumes no offsite power, onsite power, feedwater, or operator actions. Reactor coolant pump (RCP) shaft seal leakage during the TMLB' sequence was also analyzed. The core damage occurred about 7300 seconds after the transient initiated in the base TMLB' sequence. The core damage occurred earlier in TMLB' with RCP shaft seal leakage than in the base TMLB' sequence. The earlier the shaft seal failed, the earlier the core damage occurred. RELAP5/MOD2 and SCDAP/MOD1 computer codes were used in the analyses.

- Pernecky, L., G. Lzsoel, L. Szados, and I. Toth, 1990, *The Adaption of the RELAP5/MOD1 Code*, Hungarian Academy of Sciences, Budapest, Hungary, Central Research Institute for Physics, January.

Experiences with the application of RELAP5/MOD1 in evaluating the LOCA type failure simulation experiments of pressurized water reactors are presented in two parts under the same title. The simulation experiments were performed in the SPES facility (Simulator PWR per Esperienze di Sicurezza, Italy) in the framework of the Organization for Economic Cooperation and Development/Committee on Safety of Nuclear Installations International Standard Problem No. 22. The calculational procedures and the input preparation strategy for WWER-1000 type reactors are described.

- Petelin, S., I. Parzer, M. Gregoric, B. Mavko, A. Stritar, and M. Osredkar, 1989, "Post-test Calculation of SPE-2 with RELAP5/MOD2," *Technical Committee/Workshop on Computer Aided Safety Analysis, Berlin, German Democratic Republic, April 1989, In Computer Aided Safety Analysis, 1989*, Institut Jozef Stefan Ljubljana, Yugoslavia.

The PMK-NVH test facility was selected for the International Atomic Energy Agency (IAEA) SPE-2 Standard Problem. This facility has a high-pressure hydraulic loop containing an electrically heated reactor core, steam generator, primary pump, high-pressure safety injection system, and low-pressure safety injection accumulators. A small break loss-of-coolant accident was simulated. Results presented in this paper were obtained by posttest calculation. Calculations were performed by the RELAP5/MOD1/025 IBM version and by the RELAP5/MOD2/36.00 VAX version using the same input model, rearranged only slightly for different input requirements for different program versions.

- Plessinger, M. P., 1985, *Quick Look Report for Semiscale MOD-2C Test S-FS-11*, EGG-RTH-7103, November.

Results of a preliminary analysis of the fifth test performed in the Semiscale MOD-2C Steam Generator Feedwater and Steam Line Break (FS) experiment series are presented. Test S-FS-11 simulated a pressurized water reactor transient initiated by a 50% break in a steam generator bottom feedwater line downstream of the check valve. With the exception of primary pressure, the initial conditions represented the initial conditions used for the Combustion Engineering, Inc. System 80 Final Safety Analysis Report Appendix 15B calculations. The transient included an initial 600-s period in which only automatic plant protection systems responded to the initiating event. This period was followed by a series of operator actions necessary to stabilize the plant followed by break isolation and affected loop steam generator refill with auxiliary feedwater. The test results provided a measured evaluation of the effectiveness of the automatic responses in minimizing primary system overpressurization and operator actions in stabilizing the plant. Test data were compared with the RELAP5/MOD2 computer code and also provided a basis for comparison with other tests in the series of the effects of break size on primary overpressurization and primary-to-secondary heat transfer.

Ransom, V. H., 1989, *Numerical Modeling of Two-Phase Flows*, EGG-EAST-8546, May.

This course is designed to provide an introduction to the application of two-fluid modeling techniques to two-phase or, more generally, multiphase flows, and to the numerical methods that have been developed for the solution of such problems. The methods that are presented have evolved to a large extent as a result of international efforts to improve the understanding of light water reactor transient response to postulated loss-of-coolant accidents. Transient simulation codes that are based on these methods are now in routine use throughout the international light water reactor safety research and regulatory organizations.

While modeling methods for two-phase flow have evolved to the point that it is possible to predict the behavior of nuclear power plants under a wide variety of transient situations, the state of two-phase modeling has not progressed to the point of true predictive capability. The material that is presented in this course represents, to the best of the author's knowledge, the state of the art in modeling two-phase transient processes in light water reactor nuclear power systems. The material is based on experience accumulated by the author in the course of developing the RELAP5 computer code for simulating the transient behavior of light water reactor systems under normal operation and postulated accident conditions such as loss-of-coolant accidents.

Ransom, V. H., et al., 1985, *RELAP5/MOD2 Code Manual Volume 1: Code Structure, System Models, and Solution Methods*, NUREG/CR-4312, EGG-2396, August.

Ransom, V. H., et al., 1985, *RELAP5/MOD2 Code Manual Volume 2: Users Guide and Input Requirements*, NUREG/CR-4312, EGG-2396, December.

The principal objective of the RELAP5 project is to provide the U.S. Nuclear Regulatory Commission with a fast running and user convenient light water reactor system transient analysis code for use in rule making, licensing audit calculations, evaluating operator guidelines, and as a basis for a nuclear plant analyzer. The RELAP5/MOD2 code has been



developed for best-estimate transient simulation of pressurized water reactors and associated systems. The code modeling capabilities are simulation of large and small break loss-of-coolant accidents, as well as operational transients such as anticipated transient without Scram, loss of offsite power, loss of feedwater, and loss of flow. A generic modeling approach uses as much of a particular system to be modeled as necessary. RELAP5/MOD2 extends the modeling base and capabilities offered by previous versions of the code. In particular, MOD2 contains two energy equations, reflood heat transfer, a two-step numerics option, a gap conductance model, revised constitutive models, and additional component and control system models. Control system and secondary system components have been added to permit modeling of plant controls, turbines, condensers, and secondary feedwater conditioning systems. The modeling theory and associated numerical schemes are documented in Volume 1 to acquaint the user with the modeling base and thus aid in effective use of the code. Volume 2 contains detailed instructions for code application and input data preparation. In addition, Volume 2 contains user guidelines that have evolved over the past several years from application of the code at the Idaho National Engineering Laboratory and other national laboratories, and by industry users throughout the world.

Ransom, V. H., 1983, "RELAP5/MOD2: For PWR Transient Analysis," *International Conference on Numerical Methods in Nuclear Engineering, Montreal, Canada, September 6, 1983, August.*

RELAP5 is a light water reactor system transient simulation code for use in nuclear plant safety analysis. Development of a new version RELAP5/MOD2, has been completed and will be released to the U.S. Nuclear Regulatory Commission during September 1983. The new and improved modeling capability of RELAP5/MOD2 is described and some developmental assessment results are presented. The future plans to extend the code to include severe accident modeling are briefly discussed.

Ransom, V. H., and V. Mousseau, 1990, "Convergence and Accuracy Expectations for Two-Phase Flow Simulations," *1990 Canadian Nuclear Society International Conference on Simulation Methods in Nuclear Engineering, Montreal, Canada, April 18-20, 1990.*

The convergence and accuracy of the RELAP5/MOD2 two-phase flow model is studied by using analytical arguments, simple test problems, and comparison with results using a totally hyperbolic two-fluid model. The results of this study indicate that the basic two-fluid model, as numerically implemented in RELAP5/MOD2, is consistent, stable, and convergent. When constitutive models are included to obtain an engineering model for two-phase flow, convergence is obtained for discretizations that are consistent with the modeling uncertainty. Small irregularities in the solutions were observed at the finest discretizations. These irregularities are due to the constitutive models and/or their numerical implementation, but remain well within the two-phase flow model uncertainties.



Ransom, V. H., and J. D. Ramshaw, 1988, "Discrete Modeling Considerations in Multiphase Fluid Dynamics," *Third International Topical Meeting on Nuclear Power Plant Thermal Hydraulics and Operations, Seoul, Korea, November 1988.*

A discussion is given of discrete modeling considerations in multiphase fluid dynamics and related areas. By the term "discrete modeling" the authors refer to a collection of ideas and concepts that they hope will ultimately provide a philosophical basis for a more systematic approach to the solution of practical engineering problems using digital computers. As presently constituted, the main ingredients in the discrete modeling "Weltanschauung" are made up of five considerations. First, any physical model must eventually be cast into discrete form to be solved on a digital computer. Second, the usual approach of formulating models in differential form and then discretizing them is an indirect route to a discrete model. It is also potentially hazardous: the length and time scales of the discretization may not be compatible with those represented in the model. Therefore, it may be preferable to formulate the model in discrete terms from the outset. Third, computer time and storage constraints limit the resolution that can be employed in practical calculations. These limits effectively define the physical phenomena, length scales, and time scales, which cannot be directly represented in the calculation and therefore must be modeled. This information should be injected into the model formulation process at an early stage. Fourth, practical resolution limits are generally so coarse that traditional convergence and truncation-error analyses become irrelevant. Fifth, a discrete model constitutes a *reduced description* of a physical system from which fine-scale details are eliminated. This elimination creates a closure problem, which has an inherently statistical character because of the uncertainty about the missing details. Methods from statistical physics may therefore be useful in the formulation of discrete models. In the present paper, the authors elaborate on these themes and illustrate them with simple examples.

The modeling of multiphase flow plays a fundamental role in light water reactor safety because of the impossibility of testing power reactors under all regimes of operation that might exist as a result of hypothetical accidents. System simulation codes such as RELAP5 and TRAC have been developed for use in predicting the response of reactor systems to design basis accidents, and they rely heavily on multiphase flow modeling. The development and assessment of these codes continue to be the focus of significant worldwide attention. Even so, these models for multiphase flow can not be regarded as entirely satisfactory for either an accuracy or a computing speed. The lesser used detailed multidimensional codes such as COBRA and COMMIX suffer similar deficiencies.

Riemke, R. A., 1989, *Horizontal Flow Stratification Modifications for RELAP5/MOD3*, EGG-EAST-8526, February.

The report documents the modifications to the horizontal stratification model in RELAP5/MOD3. Background information, the model description and solution method, coding changes, and an assessment of these changes are described in the report. The use of the phasic velocity difference in the Taitel-Dukler criterion along with a mass flux criterion improved the void fraction data comparison for the Two-Phase Flow Test Facility tests. Modifications and error corrections to the void gradient term improved the code's capability to calculate the correct velocities.

Rinckel, M. A., and R. J. Schomaker, 1986, *RELAP5/MOD2 Benchmark of OTIS Leak Size Test #2202AA*, BAW-1092, January.

This benchmark of the RELAP5/MOD2 code using OTIS Test #2202AA was performed to demonstrate the capabilities of the RELAP5/MOD2 code to predict the phenomena characteristic of a small break loss-of-coolant transient. This report is produced as partial fulfillment of the Babcock & Wilcock Owners Group commitment to the Integral System Test Program. The Once-Through Integral System (OTIS) facility, was designed and built for the investigation of thermal hydraulic phenomena associated with small break loss-of-coolant accidents (SBLOCAs). The facility is a one-loop (one hot leg, one steam generator, and one cold leg) scaled representation of a B&W 205 Fuel Assembly raised loop plant. In March 1984, OTIS test 2202AA, which consisted of a 15 cm<sup>2</sup> pump suction SBLOCA with the pressurizer isolated and guard heaters energized, was completed. Important SBLOCA phenomena observed included system saturation, intermittent two-phase natural circulation, high elevation and pool boiler condenser modes of cooling, and system refill. The objective of this analysis was to simulate OTIS test 2202AA, up to and including the pool boiler condenser mode of cooling, with the current B&W version of RELAP5/MOD2/36. A model noding diagram is presented. The hot leg U-bend and steam generator noding are consistent with the modeling used for the Multiloop Integral System Test facility. A detailed description of the OTIS facility in parallel with a discussion of the RELAP5 model is presented are also given. The results of the study and concluding comments are also given.

Rohatgi, U. S., P. Saha, and V. K. Chexal, 1985, "Considerations for Realistic ECCS Evaluation Methodology for LWRs," *Third International Meeting on Reactor Thermal Hydraulics, Newport, Rhode Island, October 1985*, BNL-NUREG-37036, *Nuclear Technology*, 76, 1, pp. 11-26.

Various phenomena that govern the course of large and small break loss-of-coolant accidents in light water reactors and affect the key parameters (e.g., peak cladding temperature; timing of the end of blowdown, beginning of reflood, and complete quench) have been identified. The models and correlations for these phenomena in the current literature, in advance codes, and as prescribed in the current emergency core cooling system methodology outlined in Appendix K of Code of Federal Regulations 50 have been reviewed. It was found that the models and correlations in the present best-estimate codes such as TRAC and RELAP5 could be made more realistic by incorporating some of these models from the literature. However, an assessment program will be needed for the final model selection for the codes.

Rosdahl, O., and D. Caraher, 1986, *Assessment of RELAP5/MOD2 Against Critical Flow Data from Marviken Tests JIT 11 and CFT 21*, NUREG/IA-0007, STUDSVIK/NP-86/99, September, Studsvik Energiteknik AB.

RELAP5/MOD2 simulations are reported for the critical flow of saturated steam, the critical flow of subcooled liquid, and a low quality two-phase mixture. The experiments which were simulated used nozzle diameters of 0.3m and 0.5m. RELAP5 overpredicted the experimental flow rates by 10 to 25 percent unless discharge coefficients were applied.

NOTE: This report is restricted to International Code Assessment Program members unless specific permission is granted by the author.

Rosdahl, O., and D. Caraher, 1986, *International Agreement Report: Assessment of RELAP5/MOD2 Against Marviken Jet Impingement Test 11 Level Swell*, NUREG/IA-0006, September, Swedish Nuclear Power Inspectorate.

RELAP5/MOD2 simulations are reported for level swell of saturated liquid in a large vessel (5 m in diameter, 22-m high). For certain nodalizations, RELAP5 is shown to predict the measured void fraction profile with fair accuracy. RELAP5 results are shown to be dependent on nodalization, with the accuracy of computed results deteriorating significantly when a large number of nodes is employed.

Ruggles, A. E., and D. G. Morris, 1989, "Thermal-Hydraulic Simulation of Natural Convection Decay Heat Removal in the High Flux Isotope Reactor (HFIR) Using RELAP5 and TEMPEST: Part 2, Interpretation and Validation of Results," *RELAP5 Users Seminar, College Station, Texas, January 1989*.

The RELAP5/MOD2 code was used to predict the thermal hydraulic behavior of the High Flux Isotope Reactor (HFIR) core during decay heat removal through boiling natural circulation. The low system pressure and low mass flux values associated with boiling natural circulation are far from conditions for which RELAP5 is well exercised. Therefore, some simple hand calculations are used to establish the physics of the results. The interpretation and validation effort is divided between the time average flow conditions and the time varying flow conditions. The time average flow conditions are evaluated using a lumped parameter model and heat balance. The Martinelli-Nelson correlations are used to model the two-phase pressure drop and void fraction vs. flow quality relationship within the core region. Systems of parallel channels are susceptible to both density wave oscillation and pressure drop oscillations. Periodic variations in the mass flux and exit flow quality of individual core channels are predicted by RELAP5. These oscillations are consistent with those observed experimentally and are of the density wave type. The impact of the time varying flow properties on local wall superheat is bounded herein. The conditions necessary for Ledinegg flow excursions are identified. The conditions do not fall within the envelope of decay heat levels relevant to HFIR in boiling natural circulation.

Salim, F., and Y. A. Hassan, 1988, "A RELAP5/MOD2 Model of a Nuclear Power Plant and Sensitivity Study on the Nodalization Scheme," *Transactions of the American Nuclear Society 57, Joint Meeting of the European Nuclear Society and the American Nuclear Society, Washington, D.C., 1988*.

The complex nature of nuclear power plants makes it essential to have an extensive understanding of its behavior under various operation conditions. One of the analysis methods is to perform simulations on system computer codes. These codes provide the analyst with a tool to predict the system behavior under normal and abnormal conditions. Prior information obtained from such analyses becomes of paramount importance in designing and operating a nuclear power system. The purpose of this study was to develop

a RELAP5/MOD2 model of a nuclear power plant and conduct a sensitivity study on the nodalization scheme. Favorable agreement was obtained.

Sandervag, O., 1987, "Swedish Experience with RELAP5/MOD2 Assessment," *14th Water Reactor Safety Information Meeting, Gaithersburg, Maryland, October 27, 1986*, NUREG-CP-0082, Volume 5, pp. 117-132, February, Studsvik Energiteknik AB, Nykoping, Sweden.

The Swedish assessment of RELAP5/MOD2 is a part of the International Code Assessment Program, which is organized by the U.S. Nuclear Regulatory Commission. The major part of the experimental data used for assessment is of Swedish origin. The data encompass critical-flow-at-level-swell data from the Marviken facility. A part of the agreed assessment matrix has been completed. Comparison with boiling water reactor integral test data show that the major phenomena that control the core cooling during intermediate and large break loss-of-coolant accidents are qualitatively reproduced by RELAP5. Assessment against separate and integral experiments shows that the dominant uncertainty in presentation of clad temperatures is due to a poor calculation of dryout. Predicted post dryout wall temperatures, given the experiment dryout location as input parameter, generally agree well with data. Simulations of level swell following depressurization of the large diameter Marviken vessel showed that RELAP5/MOD2 was able to calculate overall axial void profiles in fair agreement with data. The assessment indicated that increasing the modeling detail could give rise to numerical instabilities. Assessment against large-scale critical flow data revealed that the agreement with data was somewhat dependent on upstream fluid conditions and modeling. Low quality two-phase flow was, in general, accurately predicted while subcooled liquid flow and saturated steam flow were generally overpredicted if no discharge coefficient was applied.

Sandervag, O., 1986, "Assessment and Application of RELAP5/MOD2 at STUDSVIK, Use of TRAC-PF1/MOD1 to Analyze Loss-of-Grid Transients," *13th Water Reactor Safety Information Meeting, Washington, D.C., October 1985*, NUREG/CP-0072, Volume 5, February, Studsvik Energiteknik AB.

The Swedish assessment plans for the advanced computer codes RELAP5/MOD2 and TRAC-PF1 are presented. RELAP5/MOD2 is based on data from experiments of mainly Swedish origin. Preliminary assessment results indicate that predictions of dryout locations and post-CHF temperatures have been improved in MOD2 as compared to MOD1. TRAC-PF1/MOD1 will be assessed using loss of external grid plant transients. One such test with improved instrumentation was conducted in Ringhal's 4 in September 1985.

Sardh, L., and K. M. Becker, 1986, *Assessments of CHF Correlations Based on Full-Scale Rod Bundle Experiments*, February, Royal Institute of Technology Stockholm.

In the present study the Barnett, Becker, Biasi, CISE-4, XN-1, Electric Power Research Institute (EPRI), and Bezrukov burnout correlations have been compared with burnout measurements obtained with full-scale 81, 64, 36 and 37-rod bundles. The total power and local power hypotheses were employed for the comparisons. The results clearly indicated that the Biasi and CISE-4 correlations do not predict the burnout conditions in full-scale rod bundles. Since these correlations yield non-conservative results, their use in computer



programs such as RELAP, TRAC, or NORA should be avoided. Considering that the effects of spacers were not included in the predictions, the Becker and Bezrukov correlations were in excellent agreement with the experimental data. However, it should be pointed out that the Bezrukov correlation only covered the 70 and 90 bar data, while the Becker correlation agreed with the experimental data in the whole pressure range between 30 and 90 bar. The Barnett, XN-1 and EPRI correlations were also in satisfactory agreement with the experiments. The authors concluded that for predictions of the burnout conditions in full-scale boiling water reactor fuel bundles, the Becker correlation should be employed.

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Schultz, R. R., Y. Kukita, and K. Tasaka, 1984, *Simulation of a TMI-2 Type Scenario at the ROSA-IV Program's Large Scale Test Facility: A First Look*, JAERI-M-84-176, September, Japan Atomic Energy Research Institute.

The Three-Mile Island-2 (TMI-2) type scenario in a Westinghouse (W) type four loop pressurized water reactor (PWR) was studied in preparation for upcoming tests in the ROSA-IV Program's Large Scale Test Facility (LSTF). The LSTF is a 1/58 scale simulator of a W-type four loop PWR with full-scale component elevation differences. TMI-2 scenario simulation analyses were conducted to establish a pretest prediction database for RELAP5 LSTF's capability to simulate the reference PWR. The basis for such RELAP5 calculations and the similarities between the LSTF and reference PWR thermal hydraulic behaviors during a TMI-2 type scenario are presented.

Schultz, R. R., Y. Kukita, Y. Koizumi, and K. Tasaka, 1984, "LSTF Simulation of the TMI-2 Scenario in a Westinghouse Type Four Loop PWR," *International Meeting on Thermal Nuclear Reactor Safety, Karlsruhe, Federal Republic of Germany, September 1984*, KFK-3880/1, pp. 467-476, Japan Atomic Energy Research Institute.

The scenario was studied in preparation for upcoming tests in the ROSA-IV Program's Large Scale Test Facility (LSTF). The LSTF is a 1/48 scale simulator of a W type four-loop pressurized water reactor (PWR) with full-scale component elevation differences. Three-Mile Island (TMI)-2 scenario simulation analyses were conducted to establish a pretest prediction database for RELAP5 code evaluation purposes and furnish a means of evaluating the LSTF's capability to simulate the reference PWR. The basis for such RELAP5 calculations and the similarities between the LSTF and reference PWR thermal hydraulic behavior during a TMI-2 scenario are presented.

Shaw, R. A., and C. B. Davis, 1990, "Simulation of Three-Dimensional Hydrodynamic Components With a One-Dimensional Transient Analysis Code," *American Nuclear Society 1990 Winter Annual Meeting, Washington, D.C., November 1990*.

The RELAP5 series of transient analysis codes was developed to provide the U.S. Nuclear Regulatory Commission with a fast running and user convenient reactor analysis tool. Although it was developed primarily for best-estimate transient simulation of pressurized



water reactors, it has been used to simulate a wide spectrum of hydraulic and thermal transients in both nuclear and non-nuclear systems involving steam-water-noncondensable fluid mixtures. In recent years, it has also been applied to thermal hydraulic analyses of various U.S. Department of Energy production reactors. RELAP5 is a one-dimensional code, meaning that the basic field equations are solved only in the axial direction of a component. Thus, for example, only axial flow is calculated in a reactor vessel; radial and azimuthal flows are not considered. This has been a minor limitation of the code because most hydraulic situations in reactor systems can be modeled adequately with a one-dimensional code. In those situations where three-dimensional flows were anticipated, the TRAC-PF1 code has generally been used. (TRAC-PF1 has the capability to model three-dimensional components; however, that option is normally only used in the reactor vessel model.) This paper describes the RELAP5 hexagonal model of the Savannah River Site (SRS) L-Reactor and comparisons of benchmark calculations with SRS data. Emphasis is placed on the multidimensional phenomena.

Shaw, E. A., and D. G. Hall, 1985, *Pre-test Analysis Document for Test S-FS-6*, EGG-SEMI-6878, May.

This report documents the pretest analyses completed for Semiscale Test S-FS-6. This test simulated a transient initiated by a 100% break in a steam generator bottom feedwater line downstream of the check valve for a Combustion Engineering, Inc. System 80 nuclear power plant. Predictions of transients resulting from feedwater line breaks in these plants have indicated that significant primary system overpressurization may occur. The enclosed analyses include a RELAP5/MOD2.2 code calculation and preliminary results from a facility hot integrated test that was conducted to near S-FS-6 specifications. The results of these analyses indicate that the test objectives for Test S-FS-6 can be achieved. The primary system overpressurization will pose no threat to personnel or plant integrity.

Shaw, R. A., S. Z. Rouhani, T. K. Larson, and R. A. Dimenna, 1988, *Development of a Phenomena Identification and Ranking Table (PIRT) for Thermal-Hydraulic Phenomena during a PWR Large Break LOCA*, EGG-2527, November.

The U.S. Nuclear Regulatory Commission (NRC) is proposing to amend its regulations to permit the use of best-estimate safety analysis codes to demonstrate that the emergency core cooling system would protect the reactor core during a postulated loss-of-coolant accident (LOCA). A key feature of this proposed rule is that the licensee will be required to quantify the uncertainty of the best-estimate calculations and include that uncertainty when comparing the calculated results with the Appendix K limits. The NRC has further proposed a code scaling, applicability, and uncertainty evaluation methodology. One of the cornerstones of that methodology is the identification and ranking of all the processes that occur during a specific scenario. The ranking is done according to importance during the scenario and is used to limit the uncertainty analysis to a sufficient but cost effective scope. The work reported in this document identifies the thermal hydraulic phenomena that occur during a large-break LOCA in a Westinghouse four-loop pressurized water reactor and ranks the relative importance of each with respect to peak cladding temperature.

programs such as RELAP, TRAC, or NORA should be avoided. Considering that the effects of spacers were not included in the predictions, the Becker and Bezrukoz correlations were in excellent agreement with the experimental data. However, it should be pointed out that the Bezrukoz correlation only covered the 70 and 90 bar data, while the Becker correlation agreed with the experimental data in the whole pressure range between 30 and 90 bar. The Barnett, XN-1 and EPRI correlations were also in satisfactory agreement with the experiments. The authors concluded that for predictions of the burnout conditions in full-scale boiling water reactor rod bundles, the Becker correlation should be employed.

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This report documents the pretest analyses completed for Semiscale Test S-FS-6. This test simulated a transient initiated by a 100% break in a steam generator bottom feedwater line downstream of the check valve for a Combustion Engineering, Inc. System 80 nuclear power plant. Predictions of transients resulting from feedwater line breaks in these plants have indicated that significant primary system overpressurization may occur. The enclosed analyses include a RELAP5/MCD2/21 code calculation and preliminary results from a facility hot integrated test that was conducted to near S-FS-6 specifications. The results of these analyses indicate that the test objectives for Test S-FS-6 can be achieved. The primary system overpressurization will pose no threat to personnel or plant integrity.

Shaw, R. A., S. Z. Rouhani, T. K. Larson, and R. A. Dimenna, 1988, *Development of a Phenomena Identification and Ranking Table (PIRT) for Thermal-Hydraulic Phenomena during a PWR Large Break LOCA*, EGG-2527, November.

The U.S. Nuclear Regulatory Commission (NRC) is proposing to amend its regulations to permit the use of best-estimate safety analysis codes to demonstrate that the emergency core cooling system would protect the reactor core during a postulated loss-of-coolant accident (LOCA). A key feature of this proposed rule is that the licensee will be required to quantify the uncertainty of the best-estimate calculations and include that uncertainty when comparing the calculated results with the Appendix K limits. The NRC has further proposed a code scaling, applicability, and uncertainty evaluation methodology. One of the cornerstones of that methodology is the identification and ranking of all the processes that occur during a specific scenario. The ranking is done according to importance during the scenario and is used to limit the uncertainty analysis to a sufficient but cost effective scope. The work reported in this document identifies the thermal hydraulic phenomena that occur during a large-break LOCA in a Westinghouse four-loop pressurized water reactor and ranks the relative importance of each with respect to peak cladding temperature.

Shinozawa, N., M. Fujisaki, M. Makino, K. Kondou, and M. Ishiguro, 1987, *Conversion Tool for the LWR Transient Analysis Code RELAP5 from the CDC Version to the FACOM Version*, JAERI-M-86-186, January, Japan Atomic Energy Research Institute, Tokyo.

The light water reactor transient analysis code RELAP5 was developed on the Control Data Corporation (CDC)-CYBER 176 at the Idaho National Engineering Laboratory. The RELAP5 code has often been updated to extend the analyzing model and correct the errors. At the Japan Atomic Energy Research Institute, the code was converted from the CDC version to the FACOM version and the converted code was used. The conversion consumes a lot of time because the code is large and there is a difference between CDC and FACOM machines. To convert the RELAP5 code automatically, the software tool was developed. By using this tool, the efficiency for converting the RELAP5 code was improved. Productivity of the conversion is increased about 2.0 to 2.6 times in comparison with the manual. The procedure of conversion by using the tools and the option parameters of each tool are described.

Shumway, R. W., 1989, *New Critical Heat Flux Method for RELAP5/MOD3*, EGG-EAST-8443, January.

The RELAP5/MOD2 computer program has been criticized for using the Biasi correlation to predict the critical heat flux in rod bundles when the correlation is based on tube data. In addition, the Royal Institute of Technology in Sweden tested MOD2 against their tube data and found it to generally overpredict the value of the critical heat flux. This report discusses the updates that result in MOD3 using the 1986 Atomic Energy of Canada, Limited-University of Ottawa table lookup method for critical heat flux. The table is made from tube data but has multiplying factors to allow application to rod bundles. In addition, it considers both forward and reverse flow and the effect of boundary layer changes at both the bundle inlet and behind grid spacers. The new model has been tested against both tube and rod bundle data. Generally, the results are better with the new model particularly in the mid-mass flux range.

Shumway, R. W., J. R. Larson, and J. L. Jacobson, 1988, *Applicability of RELAP5/MOD2 to N Reactor Safety Analysis Part 1 -- Quick Look Evaluation*, EGG-TFM-8026, February.

This report is Part 1 of a two-part evaluation of the ability of the RELAP5 computer code to calculate N Reactor transients. The RELAP5/MOD2 computer code, in modified form, has been used by EG&G Idaho, Inc. and Westinghouse Hanford to model hypothetical N Reactor transients. Because RELAP5/MOD2 was developed primarily to model commercial pressurized water reactors, which have vertical fuel channels, its ability to accurately calculate the thermal hydraulic phenomena in N Reactor type horizontal fuel channels has never been assessed. Part 1 of this study relies on readily available modeling information, and Part 2 involves obtaining horizontal channel data and making new calculations and data comparisons.

Sjoeborg, A., and D. Caraher, 1986, *Assessment of RELAP5/MOD2 Against 25 Dryout Experiments Conducted at the Royal Institute of Technology*, NUREG/IA-0009, October, Swedish Nuclear Power Inspectorate.

RELAP5/MOD2 simulations of post-dryout heat transfer in a 7-m long, 1.5-cm diameter heated tube are reported. The Biasi critical heat flux correlation is shown to be inadequate for predicting the experimental dryout. RELAP5 accurately predicted the measured temperatures downstream of the dryout once it was forced to predict dryout at the experimentally measured location.

Slovik, G. C., U. S. Rohatgi, J. Jo, 1990, *RELAP5/MOD2.5 Analysis of the HFBR [High Flux Beam Reactor] for a Loss of Power and Coolant Accident*, BNL-52243, May.

A set of postulated accidents were evaluated for the High Flux Beam Reactor (HFBR) at Brookhaven National Laboratory. A loss-of-power accident (LOPA) and a loss-of-coolant accident were analyzed. This work was performed in response to a U.S. Department of Energy review that wanted to update the understanding of the thermal hydraulic behavior of the HFBR during these transients. These calculations were used to determine the margins to fuel damage at the 60-MW power level. The LOPA assumes all the backup power systems fail (although this event is highly unlikely). The reactor scrams, the depressurization valve opens, and the pumps coast down. The HFBR has downflow through the core during normal operation. To avoid fuel damage, the core normally goes through an extended period of forced downflow after a scram before natural circulation is allowed. During a LOPA, the core will go into flow reversal once the buoyancy forces are larger than the friction forces produced during the pump coast down. The flow will stagnate, reverse direction, and establish a buoyancy driven (natural circulation) flow around the core. Fuel damage would probably occur if the critical heat flux (CHF) limit is reached during the flow reversal event. The RELAP5/MOD2.5 code, with an option for heavy water, was used to model the HFBR and perform the LOPA calculation. The code was used to predict the time when the buoyancy forces overcome the friction forces and produce upward directed flow in the core. The Monde CHF correlation and experimental data taken for the HFBR during the design verification phase in 1963 were used to determine the fuel damage margin.

Smethurst, A. J., 1990, *Post-Test Analysis of LOBI Test BT-12 using RELAP5/MOD2*, AEEW-R2645, April, Winfrith Technology Centre, United Kingdom Energy Authority, Winfrith, United Kingdom.

Stadtke, H., 1989, "JRC ISPRA Contribution to the Improvement of RELAP5/MOD2," *16th Water Reactor Safety Information Meeting, Gaithersburg, MD, March 1989*, Commission of the European Communities, Ispra, Italy.

The assessment of the RELAP5/MOD2 code within the framework of the International Code Assessment and Applications Program (ICAP) has identified various modeling deficiencies and a strong need for a further development of this code. For this reason, a multinational effort, coordinated by the ICAP Technical Program Group, has been started for the improvement of RELAP5/MOD2. The Joint Research Centre (JRC) Ispra



contribution to this activity is based on the experience gained from the improvement of RELAP5/MOD1. The paper summarizes several modifications and model improvements that have been implemented into a JRC Ispra version of RELAP5/MOD2. This concerns the calculations of state properties for vapor and steam, interphase drag coefficients, occurrence of stratified conditions in horizontal pipes, and critical flows for saturated (two-phase) conditions. The results of these model improvements are demonstrated by the comparison of calculated values using the original and modified versions of RELAP5/MOD2 with separate effect and integral test data.

Stadtke, H., and W. Kolar, 1988, "JRC Ispra Results from Assessment of RELAP5/MOD2 on the Basis of LOBI Test Data," *15th Water Reactor Safety Information Meeting, Gaithersburg, Maryland, October, 26, 1987*, February Commission of the European Communities, Ispra, Italy.

In the framework of the LOBI project, various RELAP5 code versions have been used extensively for test design calculations, pretest predictions and posttest analysis. Important results from assessment calculations and code sensitivity studies performed in 1986/1987 with RELAP5/MOD2 are presented in this paper. The assessment cases include small break loss-of-coolant accident and special transients experiments. From the comparison of measured and predicted parameters, conclusions are drawn on the prediction capabilities of RELAP5/MOD2. Specific problems observed with regard to the automatic time-step control, flow regime selection, interphase heat transfer, and break mass flow calculations are analyzed. The significance of these deficiencies are described and recommendations are given for the improvement of the RELAP5 code.

Stadtke, H., et al., 1987, "Post-Test Analysis of LOBI-MOD2 Special Transients Tests Using RELAP5," *American Nuclear Society Anticipated and Abnormal Transients in Nuclear Power Plants, Atlanta Georgia, April 1987*, Joint Research Centre - Ispra Establishment.

The LOBI-MOD2 integral test facility is a 1/700 scaled model of a pressurized water reactor operated at the Joint Research Centre of the European Communities in Ispra, Italy. Within the LOBI-MOD2 test program, three experiments simulating special transient scenarios in a pressurized water reactor have been performed so far: (a) loss of normal onsite and offsite power with failure of automatic scram system (Test A2-90), (b) loss of main feedwater (Test BT-00), and (c) small steam line break (Test BT-01). For all three experiments, various pretest and posttest predictions have been performed with the reactor safety codes RELAP5/MOD1-EUR, an improved version of RELAP5/MOD1, and RELAP5/MOD2. In general, the predicted system behavior shows a good qualitative and quantitative agreement with the measured data for the short-term transient (5 to 10 minutes). The relatively large deviations observed for the long-term transients (2 to 4 hours) are a result of both deficiencies in codes and uncertainties in defining second-order effects like heat losses, structural heat, bypass flows, and small leakages. In the paper, a comparison of measured and predicted key parameters will be given for all three experiments and existing discrepancies will be analyzed. Specific emphasis will be given to the codes' capabilities to describe the governing phenomena including (a) single- and two-phase natural circulation in the primary system at high pressure, (b) mismatch between power generated in the core and the heat removal by the steam generators, (c) pressurizer

insurge and fluid temperature stratification, (d) heat transfer conditions in the steam generators with reduced mass inventory on the secondary side, and (e) modeling of complex control circuits and valve operation. From the analysis of existing discrepancies between measured and predicted system behavior, recommendations will be given for a further improvement of the analytical capabilities of RELAP5 for special transient calculations.

Steinke, R., et al., 1984, "Nuclear Plant Analyzer: An Interactive TRAC/RELAP Power-Plant Simulation Program," *Proceedings of the International Conference on Power Plant Simulation, Mexico City, Mexico, November 1984.*

The Nuclear Plant Analyzer (NPA) is a computer-software interface for executing the TRAC or RELAP5 power plant systems codes. The NPA is designed to use advanced supercomputers, long-distance data communications, and a remote workstation terminal with interactive computer graphics to analyze power plant thermal hydraulic behavior. The NPA interface simplifies the running of these codes through automated procedures and dialog interaction. User understanding of simulated plant behavior is enhanced through graphics displays of calculational results. These results are displayed concurrently with the calculation. The user has the capability to override the plant's modeled control system with hardware adjustment commands. This gives the NPA the utility of a simulator and the accuracy of an advanced, best-estimate, power plant systems code for plant operation and safety analysis.

Stoop, P. M., J. P. A. VanDenBogaard, A. Woudstra, and H. Koning, 1988, "Application of RELAP5/MOD2 for Determination of Accident Management Procedures," *15th Water Reactor Safety Information Meeting, Gaithersburg, Maryland, October 26, 1987, February, Netherlands Energy Research Foundation, Petten.*

This paper presents the results of a number of severe accident transient analyses, which have been performed for the two nuclear power plants (NPPs) under operation in the Netherlands, using the RELAP5/MOD2 computer program. The two NPPs include a natural circulation boiling water reactor (BWR) of the early General Electric design, and a pressurized water reactor (PWR) of the Kraftwerk Union design. The transients considered include station blackout, anticipated transient without scram, primary feed and bleed (PWR), and intermediate break loss-of-coolant accident (BWR). All transients considered may potentially end up in a core melt situation. The influence of the operator action on the course of the transient events has been investigated, especially with respect to the possibility of depressurizing the plant before core melt actually occurs. The results of the analyses serve as input for a safety evaluation of both NPPs presently being performed as part of the post-Chernobyl activities in the Netherlands.

Streit, J. E., and W. E. Owca, 1985, *Pretest Analysis Document for Test S-NH-2, EGG-RTH-7101, November.*

This report documents the pretest calculations completed with the RELAP5/MOD2/36.01 code for Semiscale MOD-2C Test S-NH-2. The test simulated the transient that results from the shear in a small diameter penetration of a cold leg, equivalent to 2.1% of the cold leg flow area. The high-pressure injection system was assumed to be inoperative

throughout the transient. The recovery procedure consisted of latching open both steam generator atmospheric dump valves, supplying both steam generators with auxiliary feedwater, and injecting water by normal accumulator operation. The auxiliary feedwater system was assumed to be partially inoperative so the auxiliary feedwater flow was degraded. Recovery was initiated upon a peak cladding temperature of 811 K (100°F). The test was terminated when primary pressure had been reduced to the low-pressure injection system setpoint of 1.38 MPa (200 psia). The calculated results indicate that the test objectives can be achieved and the proposed test scenario poses no threat to personnel or plant integrity.

Stubbe, E. J., 1986, *International Agreement Report: Assessment Study of RELAP5/MOD2/Cycle-36.01 Based on the DOEL 2 Steam Generator Tube Rupture Incident of June 1979*, NUREG/IA-0008, October, TRACTIONEL - Brussels, Belgium.

This report presents a code assessment study based on a real plant transient that occurred at the DOEL-2 power plant in Belgium on June 25, 1979. DOEL-2 is a two-loop Westinghouse pressurized water reactor plant of 392 MWe. A steam generator tube rupture occurred at the end of a heat-up phase, which initiated a plant transient that required substantial operator involvement and presented many plant phenomena of interest for code assessment. While real plant transients are of special importance for code validation because of the elimination of code scaling uncertainties, they introduce some uncertainties related to the specifications of the exact initial and boundary conditions. These conditions must be reconstructed from available on-line plant recordings and on-line computer diagnostics. Best-estimate data have been reconstructed for an assessment study with RELAP5/MOD2/36.01. Because of inherent uncertainties in the plant data, the assessment work is focussed on phenomena where the comparison between plant data and computer data is based more on trends than on absolute values. Such an approach is able to uncover basic code weaknesses and strengths that can contribute to a better understanding of the code potential. This work was performed by TRACTIONEL, the Architect-Engineer for all DOEL plants, in cooperation with the utility EBES, which owns and runs these plants.

Stubbe, E. J., and L. Vanhoenacker, 1985, "Application of RELAP5 to Analysis of the DOEL Steam Generator Tube Rupture and Studies of the Loss of Feedwater Line Break Transients," *13th Water Reactor Safety Research Information Meeting, Washington, D. C., October 1985* TRACTIONEL, Brussels, Belgium.

The RELAP5 code has been used extensively since 1981 as the main thermal hydraulic system code at TRACTIONEL. The principle analyses concerned the DOEL 1 and 2 power plants (392 MWe, 2-loop pressurized water reactors), which are not strictly covered by the existing vendor studies. The purposes of the study were to: (a) improve the understanding of various phenomena occurring during postulated plant transients, (b) update the various emergency procedures and improve operator interventions, (c) re-analyze some accident analyses in the framework of the 10-year revision of those plants, and (d) define and analyze the pressurized thermal shock limiting transients. This paper concludes with some specific remarks about the need to freeze the code in its actual state.

Ting, P., R. Hanson, and R. Jenks, 1987, *International Code Assessment and Applications Program, Annual Report*, NUREG-1270, Volume 1, March.

This is the first annual report of the International Code Assessment and Applications Program (ICAP). ICAP was organized by the Office of Nuclear Regulatory Research, U.S. Nuclear Regulatory Commission (NRC) in 1985. ICAP is an international cooperative reactor safety research program planned to continue over a period of approximately five years. To date, eleven European and Asian countries/organizations have joined the program through bilateral agreements with NRC. Seven proposed agreements are currently under negotiation. The primary mission of ICAP is to provide independent assessment of the three major advanced computer codes (RELAP5, TRAC-PWR, and TRAC-BWR) developed by NRC. However, program activities can be expected to enhance the assessment process throughout member countries. The codes were developed to calculate the reactor plant response to transients and loss-of-coolant accidents. Accurate prediction of normal and abnormal plant response using the codes enhances procedures and regulations used for the safe operation of the plant and also provides a technical basis for assessing the safety margin of future reactor plant designs. ICAP is providing required assessment data that will contribute to quantification of the code uncertainty for each code. The first annual report is devoted to coverage of program activities and accomplishments between April 1985 and March 1987.

Tuomisto, H., 1987, *Thermal-Hydraulics of the Loviisa Reactor Pressure Vessel Overcooling Transients*, June, Imatran Voima Oy, Helsinki, Finland.

In the Loviisa reactor pressure vessel safety analyses, the thermal hydraulics of various overcooling transients have been evaluated to give pertinent initial data for fracture-mechanics calculations. The thermal hydraulic simulations of the developed overcooling scenarios have been performed using best-estimate thermal hydraulic computer codes. Experimental programs have been carried out to study phenomena related to natural circulation interruptions in the reactor coolant system. These experiments include buoyancy-induced phenomena such as thermal mixing and stratification of cold high-pressure safety injection water in the cold legs and the downcomer, and oscillations of the single-phase natural circulation. In the probabilistic pressurized thermal shock study, the Loviisa training simulator and the advanced system code RELAP5/MOD2 were used to simulate selected sequences. Flow stagnation cases were separately calculated with the REMIX computer program. The methods employed were assessed for these calculations against the plant data and Imatran Voima Oy's experiments.

Tuomisto, H., B. Mohsen, and H. Kantee, 1986, "Thermal Hydraulic Analyses of Selected Overcooling Transients in the Probabilistic PTS Study of the Loviisa Reactor Pressure Vessel," *European Nuclear Conference '86 Transactions, Geneva, Switzerland, June 1986*, Technical Research Centre of Finland.

An integral probabilistic study of pressurized thermal shock to a reactor vessel has been performed at the Loviisa Nuclear Power Station in Finland. Scenarios for all overcooling events have been developed using an event tree formalism. The Loviisa training simulator, which contains a two-phase primary circuit SMABRE model, has been used to predict the

thermal hydraulic response of the plant to selected overcooling sequences. The training simulator has been validated for overcooling transient analyses by comparing predictions with actual plant transients and by benchmark calculations with RELAP5/MOD2. Special attention has been given to prediction of flow stagnation cases.

Venhuizen, J. R., and E. T. Laats, 1988, "Development of a Full Scope Reactor Engineering Simulator," *Summer Computer Simulation Conference, Seattle, Washington, July 25, 1988*.

The Idaho National Engineering Laboratory (INEL) is pursuing the development of an engineering simulator for use by several agencies of the U.S. Government. This simulator, which is part of the INEL Engineering Simulation Center, will provide the highest fidelity simulation with initial objectives for studying augmented nuclear reactor operator training, and later objectives for advanced concepts testing applicable to control room accident diagnosis and management. The simulator is being built for the Advanced Test Reactor (ATR) located at the INEL. The ATR is a 250 MW light water nuclear reactor designed to study the effects of intense radiation on samples of reactor materials. A modernization of the reactor control room (RCR) is underway to enhance reliable and efficient operation of the reactor for the next 20 years. A new simulator facility has been constructed for the RCR to support operator training requirements. The simulator, completed in April 1988, will undergo a major upgrade by replacing the simplified core physics and fluid dynamics models with the widely used RELAP5 simulation code. When completed, the RELAP5 code will operate on a CRAY X-MP/24 computer and communicate with the ATR simulator, which is some 50 miles away. The high fidelity engineering simulator will then be used to train operators to recognize and respond to severe accident scenarios, a feature never before possible with previous simulators. The unique combination of the new simulator, communications, and computing hardware demonstrates a major product of the INEL Engineering Simulation Center.

Vuorio, P., H. Tuomisto, and J. Miettinen, 1988, "Assessment of the RELAP5 and SMABRE Phase Separation Models Against Full-Scale Loop Seal Experiments," *Third International Topical Meeting on Nuclear Power Plant Thermal Hydraulics and Operations, Seoul, Korea, November 1988*, Technical Research Centre of Finland.

Full-scale experiments of the two-phase flow behavior in the cold leg loop seal of a pressurized water reactor have been performed in Imatran Voima Oy, Finland. The results of these experiments have been used to assess the two-phase calculation capability of the thermal hydraulic system codes RELAP5/MOD1, RELAP5/MOD2, and the fast running code SMABRE. The results indicate that flow regime maps of both RELAP5 versions are not sufficiently accurate to make satisfactory code predictions. On the basis of the experimental results, an improved phase separation model is proposed for the loop seal geometry using the formulation for a two-fluid model and the drift-flux model. The drift-flux model of the SMABRE code makes modifications easier. As a result, a better correspondence with the experimental results can be obtained. The improved model was demonstrated with the SMABRE code.



Wang, J. L., J. F. Kunze, and C. J. McKibben, 1987, "LOCA Analysis of a Proposed Power Increase for MURR Using RELAP5/MOD2," *Transactions of the American Nuclear Society*, November, pp. 698-699.

The University of Missouri Research Reactor (MURR) has been licensed to operate at 10-MW power since 1974. A preliminary study to increase its present power to a much higher level ( $\approx 30$  MW) shows that this is readily achievable for steady-state operating conditions. The methods used to approach the goal of power upgrade operation include the flattening of the radial power distribution by varying the fuel loading of the plates, and the changing of operating conditions to provide a somewhat higher flow rate and greater heat exchanger capability. These changes are easily accomplished without major alternations to that portion of the primary system within the pool section of the loop. However, one of the principal considerations in the power upgrade study for licensing is the loss-of-coolant accident, which is addressed in this analysis.

Wang, S., C. Wu, and J. Wang, 1987, "Assessment of the RETRAN02/MOD3 and RELAP5/MOD2 Pressurizer Model," *Transactions of the American Nuclear Society*, November, pp. 704-705.

The pressurizer in pressurized water reactor (PWR) power plants plays an important role in determining the pressure history of the primary coolant system. Thus, accurate modeling of the pressurizer is needed to simulate overall PWR power plant behavior during transients. The purpose of this paper is to present an assessment of the pressurizer model in the RETRAN02/MOD3 and RELAP5/MOD2 codes by using data from nuclear power plants. The data are from two tests at the Maanshan power plant, one test at the Shippingport nuclear power plant, and the Three Mile Island accident. The results are shown to be in good agreement with the test data.

Waterman, M. E., C. M. Kullberg, and P. D. Wheatley, 1986, *Venting of Noncondensable Gas From the Upper Head of a B & W Reactor Vessel Using Hot Leg U-bend Vent Valves*, NUREG/CR-4488, EGG-2436, March.

This report describes RELAP5/MOD2 thermal hydraulic analyses of noncondensable gas removal from Babcock & Wilcox reactor systems before and during natural circulation conditions following a severe core damage accident. Hot leg U-bend vent valves were modeled as the principal noncondensable venting pathway. The analyses will assist the U. S. Nuclear Regulatory Commission (NRC) in determining whether three B&W plants should receive permanent exemptions from a reactor vessel upper head vent requirement.

Weaver, W. L., 1989, "Plans and Status of RELAP5/MOD3," *RELAP Users Seminar, College Station, Texas, January 30-February 3, 1989*, EGG-M-89005.

RELAP5/MOD3 is a pressurized water reactor (PWR) system analysis code being developed jointly by the U.S. Nuclear Regulatory Commission and a consortium consisting of several of the countries that are members of the International Code Assessment and Applications Program. This code development program is called the ICAP Code Improvement Program. The mission of the RELAP5/MOD3 code improvement program is

to develop a code version suitable for the analysis of all transients and postulated accidents in PWR systems including both large and small break loss-of-coolant accidents (LOCAs) as well as the full range of operational transients. The emphasis of the RELAP5/MOD3 development will be on large break LOCAs since previous versions of RELAP5 were developed and assessed for small break LOCAs and operation transient test data. The paper discusses the various code models to be improved and presents the results of work completed to date.

Weaver, W. L., 1989, "RELAP5/MOD3 Development Plan and Status," *16th Water Reactor Safety Information Meeting, Gaithersburg, Maryland, October 1988.*

RELAP5/MOD3 is a pressurized water reactor (PWR) system analysis code being developed jointly by the U.S. Nuclear Regulatory Commission and a consortium consisting of several of the countries that are members of the International Code Assessment Program. The objective of the RELAP5/MOD3 code development program is to develop a code suitable for the analysis of all transients and postulated accidents in PWR systems including both large and small break loss-of-coolant accidents as well as the full range of operational transients.

Weaver, W. L., et al, 1989, "The RELAP5/MOD3 Code for PWR Safety Analysis," *Fourth Internal Topical Meeting on Nuclear Reactor Thermal Hydraulics, Karlsruhe, West Germany, October 10-13, 1989.*

RELAP5/MOD3 is a pressurized water reactor (PWR) system analysis code being developed jointly by the U.S. Nuclear Regulatory Commission and a consortium consisting of several countries that are members of the International Code Assessment and Applications Program (ICAP). This code development program is called the ICAP Code Improvement Program. The mission of the RELAP5/MOD3 code improvement program is to develop a code version suitable for the analysis of all transients and postulated accidents in PWR systems including both large and small break loss-of-coolant accidents (LOCAs) as well as the full range of operational transients. The emphasis of the RELAP5/MOD3 development will be on large break LOCA since previous versions of RELAP5 were developed and assessed for small break LOCAs and operational transient test data. The paper discusses the various code models to be improved and presents the results of work completed to date.

Wheatley, P. D., et al., 1986, *RELAP5/MOD2 Code Assessment at the Idaho National Engineering Laboratory*, NUREG/CR-4454, EGG-2428, March.

Independent assessment of the RELAP5 code was continued with the assessment of RELAP5/MOD2 during 1985. RELAP5 was assessed using a range of integral and separate-effects data. Semiscale tests S-UT-8, S-UT-6, and S-PL-4 simulating small-break transients were used for assessment. GERDA 1605AA and Model Boiler-2 were also used. The crossflow junction capability in RELAP5 was assessed using the Electric Power Research Institute's single-phase liquid subchannel blockage test data. International Standard Problem 18 was also reviewed as part of the assessment of RELAP5/MOD2. Results of the independent assessments are documented in this report.

Winkler, F., 1986, "FRG Assessment of TRAC-PF1/MOD1 and RELAP5/MOD2," *13th Water Reactor Safety Information Meeting, Washington, D.C., October 1985*, NUREG/CP-0072, Volume 5, February, Kraftwerk Union AG, Federal Republic of Germany.

The U.S. Nuclear Regulatory Commission and Bundes Ministerium Für Forschung und Technologie (BMFT) of the Federal Republic of Germany (FRG) have established a bilateral agreement in which Kraftwerk Union (KWU) and Gesellschaft für Reaktorsicherheit (GRS) will perform 50 code assessment calculations in return for receipt of the four advanced computer codes TRAC-PF1, TRAC-BD, TRAC-BF1, and RELAP5/MOD2. This presentation describes the structure of the proposed code assessment studies and the experimental facilities and experiments to be used for these studies. The proposed studies currently include analysis of experiments in FRG experimental facilities and analysis for commissioning transients in modern KWU 1300-MW pressurized water reactor and boiling water reactor nuclear power plants. The currently proposed studies in experimental facilities use data from the Upper Plenum Test Facility, PKL, and the Karlstein Calibration test facility. Separate effects test data will primarily be used to assess individual models within the codes while integral test data will be used to assess the entire code. These assessment activities will be the FRG contribution to the International Code Assessment Program.

Winkler, F. J., and K. Wolfert, 1988, "Experience with Use of RELAP5/MOD2 and TRAC-PF1/MOD1 in the Federal Republic of Germany," *15th Water Reactor Safety Information Meeting, Gaithersburg, Maryland, October 26, 1987*, February, Siemens, KWU, Erlangen, Federal Republic of Germany.

The purpose of the Federal Republic of Germany's (FRG's) participation in the International Code Assessment and Applications Program (ICAP), with Siemens Kraftwerk Union (KWU) and Gesellschaft für Reaktorsicherheit (GRS) as executing agents of the Bundes Ministerium für Forschung und Technologie (BMFT), is primarily to establish internationally assessed and approved computer codes for accident analysis of light water reactors. In Siemens KWU RELAP5/MOD2 is used as the main thermal hydraulic code for loss-of-coolant accident (LOCA) analysis over the entire transient range. Therefore, more emphasis is placed on the updated FRG-ICAP matrix on assessing RELAP5/MOD2 for large break LOCA analysis. In KWU and GRS, TRAC-PF1 is used mainly for multidimensional pressurized water reactor-benchmark studies and research, in particular for Upper Plenum Test Facility pretest and posttest analysis. The updated FRG-ICAP matrix includes 42 specific assessment studies, with 8 yet to be defined. In the paper, the types of analysis performed in FRG at KWU and GRS using RELAP5/MOD2 and TRAC-PF1 are explained. Examples of results from RELAP5 and TRAC-PF1 calculations are also presented and significant findings discussed.

Yuann, R. Y., K. S. Liang, and J. L. Jacobson, 1987, *RELAP5/MOD2 Assessment Using Semiscale Experiments S-NH-1 and S-LH-2*, NUREG/CR-5010, EGG-2520, October.

This report presents the results of the RELAP5/MOD2 posttest assessment using two small break loss-of-coolant accident (LOCA) tests (S-NH-1 and S-LH-2), which were performed in the Semiscale MOD-2C facility. Test S-NH-1 was a 0.5% small break LOCA where the

high-pressure injection system (HPIS) was inoperable throughout the transient. Test S-LH-2 was a 5% small break LOCA involving a relatively high upper-to-downcomer initial bypass flow and nominal emergency core cooling. Through comparisons between data and best-estimate RELAP5 calculations, the capabilities of RELAP5 to calculate the transient phenomena are assessed. For S-NH-1, emphasis was placed on the capability of the code to calculate various operator actions to initiate core heatup in the absence of the HPIS. For S-LH-2, the capability of the code to calculate basic small break system response (e.g., vessel level during loop seal formation and clearing, break uncover, and primary pressure response following accumulator injection) was assessed.

APPENDIX B

EXAMPLE PRESSURIZED WATER REACTOR RELAP5  
INPUT LISTING



## APPENDIX B

### EXAMPLE PRESSURIZED WATER REACTOR RELAP5 INPUT LISTING

This appendix documents the RELAP5 input listing for an example pressurized water reactor. The example reactor is of Westinghouse design with three coolant loops. This microfiche input listing complements the discussions in Section 5 that provide general guidance for the modeling of plants. Nodalization diagrams for the model listed here appear in Section 5. Table B-1 provides an index of the input listing. Page numbers shown in the table refer to the accompanying microfiche.

**Table B-1.** index of RELAP5 input listing for the example pressurized water reactor.

Input Type	Page
Problem control	1
Minor edit	1
Variable trips	2
Logical trips	8
Hydrodynamic components	
Reactor vessel (components 1XX)	10
Loop A (components 2XX)	20
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APPENDIX C

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11. ABSTRACT (200 words or less)

The RELAP5 code has been developed for best-estimate transient simulation of light water reactor coolant systems during a severe accident. The code models the coupled behavior of the reactor coolant system and the core during a severe accident transient, as well as large and small break loss-of-coolant accidents and operational transients, such as anticipated transients without scram, loss of offsite power, loss of feedwater, and loss of flow. A generic modeling approach is used that permits as much of a particular system to be modeled as necessary. Control system and secondary system components are included to permit modeling of plant controls, turbines, condensers, and secondary feedwater conditioning systems.

RELAP5/MOD3 code documentation is divided into five volumes: Volume 1 describes modeling theory and associated numerical schemes, Volume 2 contains detailed instructions for code application and input data preparation, Volume 3 provides the results of developmental assessment cases that demonstrate and verify the models used in the code, and Volume 4 presents a detailed discussion of RELAP5 models and correlations. Volumes 1-4 are in varying stages of development. This document, Volume 5, contains guidelines that have evolved over the past several years through use of the RELAP5 code.

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-Example PWR model for RELAPS/MOD3 User's Guidelines

\* Note: The following input model is for a hypothetical Westinghouse type pressurized water reactor. Even though there are many similarities between the Example PWR and some existing reactor systems, the Example PWR should not be taken as a model of any existing system. The dimensions contained herein although similar to some existing systems, are fictitious.

```
*crdno      problem type      option
0000100      new                    trans1
-----
*crdno      inp-ctrl/run option
0000101      run
-----
*crdno      input units      output units
0000102      british                  british
-----
*crdno      time 1      time 2
0000105      20.0              30.0
-----
*crdno      noncond 1      noncond 2      noncond 3      noncond 4      noncond 5
0000110      nitrogen
```

```
*crdno and time min dt max dt ssd00 minor ed major ed restart
0000201 200.0 1.0e-6 0.05 0003 40 2000 2000
```

```
*edit no.      var name      var number
0000301      p              282010000
0000302      p              382010000
0000303      p              482010000
0000304      p              800010000
0000305      p              826010000
0000306      p              854010000
0000307      p              879010000
0000308      p              510010000
0000309      p              610010000
0000310      p              710010000
0000311      p              340010000
0000312      wflow         278010000
0000313      wflow         278020000
0000314      wflow         278030000
0000315      wflow         378010000
0000316      wflow         378020000
0000317      wflow         378030000
0000318      wflow         478010000
0000319      wflow         478020000
0000320      wflow         478030000
0000321      wflow         505000000
0000322      wflow         550000000
0000323      wflow         605000000
0000324      wflow         650000000
0000325      wflow         705000000
0000326      wflow         750000000
0000327      wflow         828000000
0000328      wflow         852000000
0000329      wflow         863000000
0000330      wflow         866000000
0000331      wflow         204010000 $vessel
0000332      wflow         304010000 $vessel
0000333      wflow         403010000 $vessel
```

```
0000334      temp         830010000 $lp htr 1
0000335      temp         830020000 $lp htr 2
0000336      temp         840010000 $lp htr 3
0000337      temp         840020000 $lp htr 4
0000338      temp         840030000 $lp htr 5
0000339      temp         854010000 $wfw pwp scin hd
0000340      temp         878010000 $lp htr 6
0000341      temp         112010000 $vessel
0000342      temp         118010000 $vessel
0000343      temp         126010000 $vessel
0000344      temp         204040000 $vessel
0000345      temp         304040000 $vessel
0000346      temp         405010000 $vessel
0000347      temp         550010000 $vessel
0000348      temp         650010000 $vessel
0000349      temp         750010000 $vessel
0000350      wflow         102020000 $vessel
0000351      wflow         100020000 $vessel
0000352      wflow         112010000 $vessel
0000353      wflow         120040000 $vessel
0000354      ctrlvar      101
0000355      ctrlvar      102
0000356      ctrlvar      103
0000357      ctrlvar      121
0000358      ctrlvar      131
0000359      ctrlvar      141
0000360      ctrlvar      60
0000361      ctrlvar      180
0000362      ctrlvar      181
0000363      ctrlvar      182
0000364      ctrlvar      183
0000365      ctrlvar      003
0000367      ctrlvar      005
0000369      ctrlvar      007
0000371      ctrlvar      506
0000372      ctrlvar      606
0000373      ctrlvar      706
0000374      ctrlvar      570
0000375      ctrlvar      670
0000376      ctrlvar      770
0000377      ctrlvar      771
0000378      ctrlvar      200
0000379      ctrlvar      202
0000380      ctrlvar      203
0000381      ctrlvar      207
0000383      ctrlvar      520
0000384      ctrlvar      629
0000385      ctrlvar      729
0000386      wflow         804000000
0000387      p              808010000
```

```
*
* trips
*
* variable trips
*
* the following trips are used to isolate the gfw sources to the three
* steam generators when carryover from the separators is 50%.
*
* trip v code 1 param 1 rel v code 2 param 2 constant latch
0000460 voidf 382010000 ge null 0 0.50
0000461 voidf 382010000 ge null 0 0.50
0000462 voidf 482010000 ge null 0 0.50
```

\* the next 2 trips are being removed so the problem will run on vax3100

\* \$cpu/real ratio .ge. 900. page 8 \*ratio changed to 900 for vax3100

\*v trip v code l param 1 rel v code 2 param 2 constant latch  
\*0000501 cntrlvar 029 ge null 0 900.0 n

\*Number of min time steps .ge. 13. page 13

\*0000502 cntrlvar 033 ge null 0 20.0 n

\*Normalized reactor power .ge. 1.08. page 16

0000503 cntrlvar 100 ge null 0 1.08 1

\*2/3 l rca with temp .le. 543f - 1/2 msiv closure. page 20

0000504 cntrlvar 111 ge null 0 2.0 n

\*1/2 avg .le. 554f - 1/2 msiv closure. page 20

0000505 cntrlvar 104 le null 0 554.0 n

\*2/3 reactor over temp delta t. page 32a

0000507 cntrlvar 180 ge null 0 2.0 1

\*2/3 reactor over power delta t. page 32a

0000508 cntrlvar 182 ge null 0 2.0 1

\*low rc flow trip. page 35a

0000509 cntrlvar 196 ge cntrlvar 187 0.0 1

\*\$pr level .le. 14.4X. page 52

0000510 cntrlvar 202 le null 0 0.144 1

\*\$pr level error 11.5X. page 53

0000511 cntrlvar 203 lt null 0 -0.05 n

\*\$pr compensated pressure error .le. 25 psi. page 53

0000512 cntrlvar 212 le null 0 -25.0 n

\*\$pr compensated pressure error .ge. 30 psi. page 54

0000513 cntrlvar 212 ge null 0 30.0 n

\*\$pr compensated pressure error .ge. 100 psi. page 54

0000514 cntrlvar 212 ge null 0 100.0 n

\*\$pr pressure .ge. 2285 psia. page 55

0000515 cntrlvar 210 ge null 0 2280.0 n

\*\$pr pressure .ge. 2350 psia. page 55

-----

0000516 cntrlvar 210 ge null 0 2350.0 n

\*\$pr pressure .ge. 2480 psia. page 56

0000517 cntrlvar 210 ge null 0 2480.0 n

\*\$pr pressure .ge. 2535 psia. page 56

0000518 cntrlvar 210 ge null 0 2535.0 n

\*\$pr level .ge. 81X. page 56a

0000519 cntrlvar 202 ge null 0 0.91 1

\*\$pr pressure .ge. 2381 psia. page 56a

0000520 cntrlvar 210 ge null 0 2381.0 1

\*\$pr pressure .le. 1859 psia. page 56a

0000521 cntrlvar 210 le null 0 1850.0 1

\*\$pr pressure .le. 1730 psia. page 56a

0000522 cntrlvar 210 le null 0 1730.0 1

\*\$pr pressure .le. 1315 psia. page 56a

0000523 cntrlvar 210 le null 0 1315.0 1

\*\$ga nr lvl .ge. 75X. page 70

0000524 cntrlvar 506 ge null 0 0.75 n

\*\$gb nr lvl .ge. 75X. page 70

0000525 cntrlvar 606 ge null 0 0.75 n

\*\$gc nr lvl .ge. 75X. page 70

0000526 cntrlvar 706 ge null 0 0.75 n

\*\$fu pump flowrate .le. 3250 gpm. page 72

0000527 cntrlvar 515 le null 0 1125.0 1

\*\$fu pump flowrate .le. 1125 gpm. page 72

0000529 cntrlvar 516 le null 0 1125.0 1

\*\$fu pump suction pressure .le. 250 psia. page 71

0000528 p 854010000 le null 0 450.0 1

\*\$hotwell mass .le. 629644.73 lbs (-12 in level). page 74

0000530 cntrlvar 518 le null 0 629644.73 1

\*\$condensate pump discharge pressure .le. 465 psia. page 74

0000531 p 926010000 le null 0 465.0 1

\*\$condensate pump trip. page 74



```

0000532 time 0 ge null 0 1.0e6 1
$plant at hot standby. page 77
-----
0000533 time 0 ge null 0 1.0e6 1
$electric power to motor driven s/w pumps available. page 76
-----
0000534 time 0 ge null 0 0.0 n
$sw discharge pressure .ie. 865 psia. page 76
-----
* v trip v code 1 param 1 rel v code 2 param 2 constant latch
0000535 cntrlvar 730 le null 0 0.0 1
$sga nr level .ie. 15% page 76
-----
0000536 cntrlvar 506 le null 0 0.15 n
$sgb nr level .ie. 15% page 76
-----
0000537 cntrlvar 806 le null 0 0.15 n
$sgc nr level .ie. 15% page 76
-----
0000538 cntrlvar 706 le null 0 0.15 n
$1/3 sg with low-ow level. page 80
-----
0000539 cntrlvar 734 ge null 0 1.0 v
$sws with 50 sec delay. page 80
-----
0000540 time 0 ge timeof 868 50.0 n
$2/3 sg with low-low level. page 81
-----
0000541 cntrlvar 734 ge null 0 2.0 n
$the following trips determine the pressure response of the steam line
$after valves. the trips are such that the valve hysteresis can be
$modeled as described in source literature.
-----
0000542 cntrlvar 554 gt null 0 0.0 n
0000543 cntrlvar 551 gt null 0 1254.0 n
0000544 cntrlvar 854 gt null 0 0.0 n
0000545 cntrlvar 651 gt null 0 1254.0 n
0000546 cntrlvar 754 gt null 0 0.0 n
0000547 cntrlvar 751 gt null 0 1254.0 n
$15% load rejection reset. page 85
-----
0000550 cntrlvar 802 ge null 0 99.70 n
$15% load rejection actuation. page 85
-----
0000551 cntrlvar 802 ge null 0 99.70 n
$35% load rejection reset. page 85
-----
0000552 cntrlvar 802 ge null 0 197.25 n

```

```

$35% load rejection actuation. page 85
-----
0000553 cntrlvar 802 ge null 0 203.25 n
$55% load rejection reset. page 85
-----
0000554 cntrlvar 802 ge null 0 304.95 n
$55% load rejection actuation. page 85
-----
0000555 cntrlvar 802 ge null 0 310.95 n
$operator override of adcs lsv control. page 82
-----
0000556 time 0 ge timeof 696 60.0 1
$adcs in steam pressure control mode. page 82
-----
0000557 cntrlvar 104 le null 0 547.0 n
$condenser pressure .11. 5 psia. page 106
-----
0000558 p 42010000 lt null 0 5.0 n
$sga steam flowrate .gt. setpoint steam flowrate. page 112
-----
0000560 cntrlvar 901 ge cntrlvar 900 0.0 n
$sgb steam flowrate .ge. setpoint steam flowrate. page 112
-----
0000561 cntrlvar 802 ge cntrlvar 900 0.0 n
$sgc steam flowrate .ge. setpoint steam flowrate. page 113
-----
0000562 cntrlvar 903 ge cntrlvar 900 0.0 n
$2/3 high steam flow. page 113
-----
0000563 cntrlvar 907 ge null 0 2.0 n
$sg low steam line pressure. page 114
-----
0000564 p 65001000 le null 0 619.0 n
$sgb low steam line pressure. page 114
-----
0000565 p 65001000 le null 0 619.0 n
$sgc low steam line pressure. page 114
-----
0000566 p 75001000 le null 0 619.0 n
$2/3 sg with low steam line pressure. page 115
-----
0000567 cntrlvar 811 ge null 0 2.0 n
$containment pressure .ge. 20 psia. page 115
-----
0000568 time 0 ge null 0 1.0e6 1
$sga high steam line differential pressure. page 116
-----
0000569 p 65001000 le p 80001000 100.0 n

```

\$sgb high steam line differential pressure. page 116

0000570 p 850010000 le p 800010000 -100.0 n

\$sgc high steam line differential pressure. page 116

0000571 p 760010000 le p 800010000 -100.0 n

\$bias high containment pressure (4 psig). page 117

0000572 time 0 ge null 0 1.0e6 l

\$turbine stop/governor valve area .le. 0.0. page 120

0000573 ctrlrvar 924 le null 0 0.0 l

\$manual turbine trip. page 120

0000574 time 0 ge null 0 1.0e6 l

\$2/3 turbine high over-temp delta t. page 121

0000575 ctrlrvar 181 ge null 0 2.0 n

\$2/3 turbine high over-power delta t. page 121

0000576 ctrlrvar 183 ge null 0 2.0 n

\$turbine runback setpoint valve area ge. 1.0. page 122

0000577 ctrlrvar 920 ge null 0 1.0 n

\$turbine valve area .le. runback setpoint valve area. page 122

0000578 ctrlrvar 924 le ctrlrvar 920 0.0 n

\$turbine valve area .le. runback setpoint area for 30 sec. page 122

0000579 time 0 ge timeof 578 30.0 n

\$sga feed/steam mismatch. page 127

0000580 wflowj 525000000 lt wflowj 555000000 -177.8 n

\$sgc feed/steam mismatch. page 127

0000581 wflowj 825000000 lt wflowj 855000000 -177.78 n

\$sgc feed/steam mismatch. page 127

0000582 wflowj 725000000 lt wflowj 755000000 -177.78 n

\$sga nr level .le. 30%. page 127

0000583 ctrlrvar 506 le null 0 0.30 n

\$sgb nr level .le. 30%. page 127

0000584 ctrlrvar 608 le null 0 0.30 n

\$sgc nr level .le. 30%. page 127

0000585 ctrlrvar 706 le null 0 0.30 n

\$manual reactor trip. page 128

0000586 time 0 ge null 0 1.0e6 l

\$ree if mass flow through mfw reg valve a is below 55.55 lbm/s

0000587 wflowj 505000000 le null 0 55.55 n

\$ree if mass flow through mfw reg valve b is below 55.55 lbm/s

0000588 wflowj 805000000 le null 0 55.55 n

\$ree if mass flow through mfw reg valve c is below 55.55 lbm/s

0000589 wflowj 705000000 le null 0 55.55 n

\$i.p. heater bypass

0000591 p 854010000 le null 0 314.7 n

0000592 p 854010000 le null 0 314.7 n

\$main feedwater pump recirculation valve trips: corresponds to 1410gpm

0000593 velj 861010000 lt null 0 3.429 n

0000594 velj 861010000 lt null 0 1.585 n

0000595 velj 864010000 lt null 0 3.429 n

0000596 velj 864010000 lt null 0 1.585 n

\$logic trips

\* remove logic \*trip 600 so problem will run on vax3100

\*1 trip trip no. 1 trip no. 2

\*0000600 501 502

\$1 trip trip no. 1 rel trip no. 2 latch comments

0000601 501 and 508 n \$comments

0000602 502 or 601 n \$trip vlv

0000603 508 and 630 n \$vlv/psp

0000604 523 and 529 n \$trcp on

0000605 511 or 512 n \$page 53

0000606 511 and 510 n \$on-off btr permissive

0000607 513 and 614 n \$porv #1 stay open

0000608 514 or 613 n \$porv #1 open. pg 54

0000609 515 and 616 n \$porv #2 stay open.

0000610 516 or 615 n \$porv #2 open. pg 55

0000611 517 and 618 n \$por #3 stay open.

0000612 518 or 617 n \$cor #1 open. p 56

0000613 524 or 625 n \$sga or b hi lvl. p 70

0000614 619 or 526 n \$cor sgc hi lvl. p 70

0000615 596 and 505 n \$ix and tr54. p 71

0000616 620 or 568 n \$1/3 hi lvl or st.

0000617 621 or 622 n \$m wlv clc w/c psp tr

0000618 622 or 529 n \$1/3 hi lvl y to scgh p

0000619 530 or 531 n \$io tr/vl or lo dschg p

0000620 624 or 625 n \$

0000621 626 or 532 n \$manual mfw pump trip

0000622 627 or 527 n \$mfw1 lo flo/mfw1 trip

0000623 627 or 528 n \$mfw2 lo flo/mfw2 trip

```

0000630 828 and 828 1 $both wfaps tripped
0000631 830 or 823 1 $sfw valves close
0000632 834 and 835 n $
0000633 839 or 840 n $
0000634 833 or 830 n $
0000635 834 and 832 n $
0000636 834 or 841 n $
0000637 836 and 835 1 $
0000642 842 or 843 n $a safety
0000643 844 or 845 n $b safety
0000644 846 or 847 n $c safety
0000650 850 and 851 n $bank 1 stay open p86
0000651 850 or 851 n $bank 1 air p 86
0000652 852 and 853 n $bank 2 stay open p86
0000653 852 or 853 n $bank 2 air p 86
0000654 854 and 855 n $bank 3 stay open
0000655 854 or 855 n $bank 3 air p 86
0000656 856 and 857 1 $trip loc to spc p 92
0000657 856 or 853 1 $hsb/spc on p 92
0000658 857 and 896 n $rx trip/loc off p 92
0000659 857 and 896 n $spc off/ra trip/pl on
0000660 904 or 867 1 $2/3 lo 1 or pr p 115
0000661 860 and 863 1 $2/3 hi xtm flo/psiv
0000662 861 or 868 1 $hi c p/psiv trip
0000663 862 and 862 n $psiv stay open p 115
0000664 869 or 870 n $a/b hi dr p 117
0000665 864 or 871 1 $or c p 117
0000666 872 or 865 n $lo pdr p/hi dr p 117
0000667 866 or 872 n $or hi cv pr p 117
0000668 867 or 861 1 $or psiv w/ocv bias
0000669 873 and 823 n $rcps on p 118
0000670 854 or 873 n $condnar trip/trip p120
0000671 870 or 896 n $or rx trip p 120
0000672 871 or 833 n $or hsb p 120
0000673 872 or 820 n $or hi sg lvl p 121
0000674 873 or 874 1 $man trip/trip p 121
0000675 875 or 876 n $irbn dt trips p 121
0000676 875 and 877 n $rbk & sp-1 p 122
0000677 875 and 879 n $rtk after 30 sec
0000678 876 or 877 n $
0000679 878 and 874 n $t viv runback p 122
0000680 880 and 883 1 $sga lvl/flo trip
0000681 881 and 884 1 $sgb lvl/flo trip
0000682 882 and 885 1 $sgc lvl/flo trip
0000683 883 or 881 1 $a or b lvl/flow
0000684 883 or 882 1 $or sgc lvl/flow
0000685 883 or 886 1 $hi per/man trip
0000686 887 or 888 1 $over-1 or p dt
0000687 885 or 886 1 $
0000688 887 or 889 1 $low rc flow
0000689 888 or 819 1 $hi pdr lvl
0000690 889 or 820 1 $hi pdr press
0000691 890 or 821 1 $in pdr press
0000692 891 or 822 1 $rcp trip
0000693 892 or 839 1 $lo sg lvl p 129
0000694 893 or 868 1 $bias
0000695 894 or 874 1 $turbine trip
0000696 895 or 884 1 $sg lvl/flow miswch
0000698 892 and 830 n $sheater drain pump trip
0000699 874 or 874 n $sheater sht supply trip

```

\*additional logic trips \*

```

*
0000701 460 and 461 n $carryover in sga sdb
0000702 701 and 462 1 $and carryover in sg c
0000703 702 and 835 n $str driven aux fw
0000704 702 and 837 n $ste driven aux fw
0000705 703 or 704 n $in sfw mode
0000706 705 and 460 1 $
0000707 706 and 706 n $close sga isolate viv
0000708 705 and 461 1 $
0000709 709 and 708 n $close sgb isolate viv
0000710 705 and 462 1 $
0000711 710 and 710 n $close sgc isolate viv
0000720 722 and 893 n $and lt 3030 gpm
0000721 720 or 894 n $or lt 1410 gpm
0000722 721 and 893 n $a pump flow low
0000724 726 and 895 n $and lt 3030 gpm
0000725 724 or 896 n $or lt 1410 gpm
0000726 725 and 895 n $b pump flow low

```

\$the following trips are necessary for steady state initialization \*  
\$and should be replaced with the proper values at the initiation of \*  
\$the transients \*

```

*v trip v code 1 para 1 rel v code 2 para 2 constant latch
0000507 cntrivar 180 ge null 0 4.0 1
0000508 cntrivar 182 ge null 0 4.0 1
0000510 cntrivar 202 le null 0 0.144 1
0000563 cntrivar 907 ge null 0 4.0 1
0000576 cntrivar 183 ge null 0 4.0 n
0000578 time 0 le null 0 0.0 n
0000541 cntrivar 734 ge null 0 4.0 1
0000575 cntrivar 181 ge null 0 4.0 n
0000577 cntrivar 920 ge null 0 12.0 n

```

```

*! trip trip no. 1 rel trip no. 2 latch comments
0000635 574 and 574 n $
0000637 574 and 574 n $
0000660 574 or 574 n $
0000674 574 or 574 n $
0000609 574 and 574 n $
0000630 574 and 574 1 $
0000531 574 and 574 1 $
0000676 574 and 574 n $
0000221 574 and 574 n $
0000628 574 and 574 n $
0000439 574 and 574 n $
0000096 574 and 574 n $

```

hydrodynamic components  
vessel  
vessel inlet annulus

```

*-----*
*crdno      component name      component type
1000000     .innamp                annulus
*
*crdno      number of volumes
1000001     3
*
*crdno      vol area            vol no.
1000101     0.0                          3
*
*crdno      length              vol no.
1000301     1.6110                        1
1000302     1.6240                        2
1000303     3.4350                        3
*
*crdno      volume              vol no.
1000401     37.306                        1
1000402     52.613                        2
1000403     60.493                        3
*
*crdno      vert angle          vol no.
1000601     90.0                          3
*
*crdno      elev change         vol no.
1000701     1.6110                        1
1000702     1.6240                        2
1000703     3.4350                        3
*
*crdno      roughness          hyd. diameter      vol no.
1000801     0.00015                    1.408                1
1000802     0.00015                    1.500                2
1000803     0.00015                    0.922                3
*
*crdno      f loss              r loss              jun no.
1000901     0.0                        0.0                  2
*
*crdno      fx                  vol no.
1001001     00                          3
*
*crdno      cabs                jun no.
1001101     0000                        2
*
*crdno      vol ic pressure      eq temp            vol no.
1001201     0      2297.4000 534.19000 1048.9000 00000000 0.0      01
1001202     0      2296.6000 534.95000 1049.0000 00000000 0.0      02
1001203     0      2295.9000 536.34000 1049.0000 00000000 0.0      03
*
*crdno      vel/flw
1001300     0
*
*crdno      f flowrate          g flowrate          j flowrate      jun no.
1001301     04702690 04702690 0.0      01      01
1001302     06188220 06188220 0.0      02      02
*
*crdno      junc dia      beta      c      #
1001401     0.922      0.      1.      1.      2
*
*-----*
* the following data represent the vessel inlet annulus fluid *
* volume below the cold leg centerline (upper volume) *
*-----*
*crdno      component name      component type
1020000     .innamp                branch

```

```

*
*crdno      6      0      number of junctions      vel/flw
1020001
*
*crdno      flow area          length              volume
1020101     0.0                    1.6110              37.306
*
*crdno      horz orient        vert orient        delta z
1020102     0.0                    -90.0               -1.6110
*
*crdno      roughness          hyd. diameter      fe
1020103     0.00015                1.408               00
*
*crdno      vol ic pressure      eq temp            00000000
1020200     0      2294.6000 533.58000 1049.1000
*
*crdno      from              to              area      f loss      r loss      cabs
1021101     102000000      106000000      0.0      0.0      0.0      0000
1021101     102010000      104000000      0.0      0.0      0.0      0000
1023101     102000000      120010000      0.0      1.37e5    1.37e5    0000
1024101     220510000      102000000      0.0      0.0      0.0      0100
1025101     220510000      102000000      0.0      0.0      0.0      0100
1026101     420610000      102000000      0.0      0.0      0.0      0100
*
*crdno      f flowrate          g flowrate          j flowrate
1021201     04700050 04700050 0.0
1022201     25.457000 25.457000 0.0
1023201     29307000 29307000 0.0
1024201     40.971000 40.971000 0.0
1025201     40.971000 40.971000 0.0
1026201     40.968000 40.968000 0.0
*
*crdno      junc dia      beta      c      #
1021110     1.408      0.      1.      1.
1022110     0.959      0.      1.      1.
1023110     1.289      0.      1.      1.
1024110     1.289      0.      1.      1.
1025110     1.209      0.      1.      1.
1026110     1.299      0.      1.      1.
*
* the following data represent the vessel inlet annulus fluid *
* volume below the cold leg centerline (lower volume) *
*-----*

```

```

*crdno      component name      component type
1040000     .nannls                branch
*
*crdno      number of junctions      vel/flw
1040001     2      0
*
*crdno      flow area          length              volume
1040101     0.0                    2.4410              67.576
*
*crdno      horz orient        vert orient        delta z
1040102     0.0                    90.0                -2.4410
*
*crdno      roughness          hyd. diameter      fe
1040103     0.00015                0.959               00
*
*crdno      vol ic pressure      eq temp            00000000
1040200     0      2297.4000 533.58000 1048.9000
*
*crdno      from              to              area      f loss      r loss      cabs
1041101     104010000      105000000      0.0      0.0      0.0      0000

```

1041101 104010000 118000000 0.0 21144. 3169. 0000

\*crdno f flowrate g flowrate j flowrate

1041201 29.932000 29.932000 0.0

1042201 20732000 20732000 0.0

\* junc dia beta c m

1041110 0.987 0. 1. 1.

1042110 0.790 0. 1. 1.

\* the following data represent the downcomer fluid volume \*

\* component name component type

1060000 downcomer annulus

\* number of volumes

1060001 7

\* vol area vol.no.

1060101 0.0 7

\* length vol.no.

1060201 2.111 6

1060302 4.094 7

\* volume vol.no.

1060401 41.560 6

1060402 162.90 7

\* vert ang vol.no.

1060601 -90.0 7

\* elev change vol.no.

1060701 -2.110 6

1060702 -4.094 7

\* roughness hyd. diameter vol.no.

1060901 0.00015 0.512 6

1060902 0.00015 0.0 7

\* f loss r loss jun.no.

1060901 0.0 0.0 6

\* fe vol.no.

1061001 90 7

\* cabs jun.no.

1061101 000 0

\* vol ic pressure eq temp vol.no.

1061201 0 2295.8000 533.59000 1048.1000 0.0000000 0.0 01

1061202 0 2296.3000 533.59000 1048.0000 0.0000000 0.0 02

1061203 0 2296.7000 533.59000 1048.0000 0.0000000 0.0 03

1061204 0 2297.1000 533.59000 1048.0000 0.0000000 0.0 04

1061205 0 2297.5000 533.59000 1048.0000 0.0000000 0.0 05

1061206 0 2297.9000 533.59000 1048.0000 0.0000000 0.0 06

1061207 0 2301.0000 533.59000 1048.7000 0.0000000 0.0 07

\* vel/flw

1061300 0

\* f flowrate g flowrate j flowrate jun.no.

1061301 29.932000 29.932000 0.0 01

1061302 29.932000 29.932000 0.0 02

1061303 29.932000 29.932000 0.0 03

1061304 29.932000 29.932000 0.0 04

1061305 29.932000 29.932000 0.0 05

1061306 29.932000 29.932000 0.0 06

\* junc dia beta c m

1061401 0.512 0. 1. 1. 6

\* the following data represent the lower plenum fluid volume \*

\* (upper volume)

\* component name component type

1100000 lowplup branch

\* number of junctions vel/flw

1100001 2 0

\* flow area length volume

1100101 0.0 5.736 484.86

\* horz orient vert orient delta z

1100102 0.0 90.0 5.736

\* roughness hyd. diameter fe

1100103 0.00015 0.0 90

\* vol ic pressure eq temp

1100200 0 2292.0000 533.59000 1048.3000 0.0000000

\* from to area f loss r loss cabs

1101101 106010000 110010000 0.0 4.70 4.70 0000

1102101 110010070 112000000 0.0 3.94 3.94 0000

\* f flowrate g flowrate j flowrate

1101201 23.326000 23.326000 0.0

1102201 10.180000 10.180000 0.0

\* junc dia beta c m

1101110 0.657 0. 1. 1.

1102110 0.6825 0. 1. 1. Hyd. Diam. of lower susp. D7.

\* the following data represent the core inlet fluid volume \*

\* component name component type

1120000 coreinl branch

\* number of junctions vel/flw

1120001 3 0

\* flow area length volume

1120101 0.0 4.094 235.90

\* horz orient vert orient delta z

1120102 0.0 90.0 4.094

\* roughness hyd. diameter fe

1120103 0.00015 0.0 30

\* vol ic pressure eq temp

1120200 0 2287.7000 533.60000 1048.0000 0.0000000



```

*
*crdno  from  to  area  f loss  r loss  cchs
1121101 11201000 11400000 0.0 2.1 2.1 0000
1122101 11601000 11201000 5.291 1.5 1.5 0000
*
*crdno  f flowrate  g flowrate  j flowrate
1121201 14.148000 14.148000 0.0
1122201 60610000 60610000 0.0
*
*  junc dia  beta  c  #
1121110 0.037 0. 1. 1.
1122110 0.790 0. 1. 1.
*

```

```

* the following data represent the core fluid volume *
*

```

```

*crdno  component name  component type
1140000  core  pipe
*
*crdno  number of volumes
1140001  6
*
*crdno  vol area  vol.no.
1140101  41.870  6
*
*crdno  jun. area  jun. no.
1140201  40.174  5
*
*crdno  length  vol.no.
1140301  2.1110  6
*
*crdno  volume  vol.no.
1140401  0.0  6
*
*crdno  vert angle  vol.no.
1140601  90.0  6
*
*crdno  elev change  vol.no.
1140701  2.1110  6
*
*crdno  roughness  hyd. diameter  vol.no.
1140801  0.00015  0.037  6
*
*crdno  f loss  r loss  jun.no.
1140901  0.59  0.59  5
*
*crdno  fe  vol.no.
1141001  00  6
*
*crdno  fvchs  jun.no.
1141101  000000  5
*
*crdno  vol ic  pressure  eq temp  vol.no.
1141201  0  2283.3000  548.50000  1049.9000  00000000 0.0  01
1141202  0  2260.3000  560.79000  1050.1000  00000000 0.0  02
1141203  0  2277.2000  574.64000  1050.3000  00000000 0.0  03
1141204  0  2274.1000  588.79000  1050.6000  00000000 0.0  04
1141205  0  2271.0000  602.50000  1050.8000  00000000 0.0  05
1141206  0  2267.9000  611.25000  1051.0000  00000000 0.0  06
*
*crdno  vel/flw
1141300  0
*

```

```

*crdno  f flowrate  g flowrate  j flowrate  jun.no.
1141301 14.889000 14.889000 0.0  01
1141302 15.142000 15.142000 0.0  02
1141303 15.406000 15.406000 0.0  03
1141304 15.689000 15.689000 0.0  04
1141305 15.989000 15.989000 0.0  05
*
*  junc dia  beta  c  #
1141401 0.019 0. 1. 1. 5 *Hyd. Diam. at grid spacer
*

```

```

* the following data represent the core bypass fluid volume *
*

```

```

*crdno  component name  component type
1160000  bypass  annulus
*
*crdno  number of volumes
1160001  6
*
*crdno  vol area  vol.no.
1160101  15.435  6
*
*crdno  length  vol.no.
1160301  2.1110  6
*
*crdno  volume  vol.no.
1160401  0.00  6
*
*crdno  vert angle  vol.no.
1160601  -90.0  6
*
*crdno  elev change  vol.no.
1160701  -2.1110  6
*
*crdno  roughness  hyd. diameter  vol.no.
1160801  0.00015  790  6
*
*crdno  f loss  r loss  jun.no.
1160901  9640.  9640.  5
*
*crdno  fe  vol.no.
1161001  00  6
*
*crdno  cchs  jun.no.
1161101  0000  6
*
*crdno  vol j:  pressure  eq temp  vol.no.
1161201  0  2296.0000  534.17000  1046.0000  00000000 0.0  01
1161202  0  2294.3000  534.68000  1049.2000  00000000 0.0  02
1161203  0  2297.5000  535.09000  1049.3000  00000000 0.0  03
1161204  0  2290.7000  535.38000  1049.4000  00000000 0.0  04
1161205  0  2299.0000  535.63000  1049.5000  00000000 0.0  05
1161206  0  2287.2000  535.58000  1049.7000  00000000 0.0  06
*
*crdno  vel/flw
1161300  0
*

```

```

*crdno  f flowrate  g flowrate  j flowrate  jun.no.
1161301 20745000 20745000 0.0  01
1161302 20756000 20756000 0.0  02
1161303 20765000 20765000 0.0  03
1161304 20773000 20773000 0.0  04
1161305 20778000 20778000 0.0  05
*
*  junc dia  beta  c  #

```

```

1161401 0.700 0. 1. 1. 5
*
* the following data represent the upper plenum fluid volume *
* below the hot leg centerline (upper volume) *
*
*crdno component name component type
1160000 uppl1c1 branch
*
*crdno number of junctions vel/flw
1160001 1 0
*
*crdno flow area length volume
1190101 0.0 2.441 225.121
*
*crdno horz orient vert orient delta z
1190102 0.0 90.0 2.4410
*
*crdno roughness hyd. diameter fe
1190103 0.00015 1.289 0
*
*crdno vol ic pressure eq temp
1180200 0 7266.1000 611.2500 1051.1000 00000000
*
*crdno from to area f loss r loss cabs
1181101 114010000 118000000 0.0 1.05 1.05 0000
*
*crdno f flowrate g flowrate j flowrate
1181201 15.612000 15.612000 0.0
*
*crdno junc dia beta c s
1181110 0.037 0. 1. 1.

```

```

* the following data represent the upper plenum fluid volume *
* below the hot leg centerline (upper volume) *
*
*crdno component name component type
1200000 uppl1c2 branch
*
*crdno number of junctions vel/flw
1200001 5 0
*
*crdno flow area length volume
1200101 0.0 1.6110 128.075
*
*crdno horz orient vert orient delta z
1200102 0.0 90.0 1.6110
*
*crdno roughness hyd. diameter fe
1200103 0.00015 1.289 00
*
*crdno vol ic pressure eq temp
1200200 0 2264.2000 610.5000 1051.3000 00000000
*
*crdno from to area f loss r loss cabs
1201101 120010000 204000000 4.577 0.0400 1.0500 0100
1202101 120010000 304000000 4.577 0.0400 1.0500 0100
1203101 120010000 404000000 4.577 0.0400 1.0500 0100
1204101 120010000 120010000 0.0 0.0 0.0 0000

```

```

1205101 118010000 120000000 0.0 4.1 4.1 0000
*
*crdno f flowrate g flowrate j flowrate
1201201 47.436000 47.436000 0.0
1202201 47.451000 47.451000 0.0
1203201 47.429000 47.429000 0.0
1204201 10648000 10648000 0.0
1205201 8.0900000 8.0900000 0.0
*
*crdno junc dia beta c s
1201110 1.211 0. 1. 1.
1202110 1.211 0. 1. 1.
1203110 1.211 0. 1. 1.
1204110 1.289 0. 1. 1.
1205110 1.289 0. 1. 1.

```

```

* the following data represent the upper plenum fluid volume *
* above the hot leg centerline *
*
*crdno component name component type
1220000 upplup pipe
*
*crdno number of volumes
1220001 3
*
*crdno vol area vol no.
1220101 0.0 3
*
*crdno length vol no.
1220301 3.435 1
1220302 1.824 2
1220303 1.611 3
*
*crdno volume vol no.
1220401 325.846 1
1220402 171.964 2
1220403 128.075 3
*
*crdno vert angle vol no.
1220601 90.0 2
*
*crdno elev change vol no.
1220701 3.435 1
1220702 1.824 2
1220703 1.611 3
*
*crdno roughness hyd. diameter vol no.
1220801 0.00015 1.289 3
*
*crdno f loss r loss junc no.
1220901 0.0 0.0 2
*
*crdno fe vol no.
1221001 00 3
*
*crdno frcabs junc no.
1221101 00100 2
*
*crdno vol ic pressure eq temp vol no.
1221201 0 2262.7000 600.6200 1051.4000 00000000 0.0 01
1221202 0 2263.5000 600.5000 1051.3000 00000000 0.0 02
1221203 0 2264.0000 600.4100 1051.3000 00000000 0.0 03

```

```

*crdno vel/flw
1221300 0
*
*crdno f flowrate g flowrate j flowrate jun.no.
1221301 .08982550 .08982550 0.0 01
1221302 .10650000 .10650000 0.0 02
*
* crdno jun dia beta c m
1221401 1.289 0. 1. 1. 2
*

```

```

* the following data represent the upper head fluid volume *
* (lower volume)
*

```

```

*crdno component name component type
1260000 upheadd2 branch
*
*crdno number of junctions vel/flw
1260001 2 0
*
*crdno flow area length volume
1260101 0.0 6.72150 513.640
*
*crdno horz orient vert orient delta z
1260102 0.0 -90.0 -6.72150
*
*crdno roughness hyd. diameter fe
1260103 0.00015 0.0 00
*

```

```

*crdno vol ic pressure eq temp
1260200 0 2261.0000 600.82000 1051.4000 .00000000
*
*crdno from to area f loss r loss cabs
1261101 126010000 126010000 0.0 1.1000e6 1.1000e6 0000
1262101 126010000 122000000 0.0 6.310e3 6.310e3 0000
*

```

```

*crdno f flowrate g flowrate j flowrate
1261201 .08190080 .08190080 0.0
1262201 .11087000 .11087000 0.0
*
* crdno jun dia beta c m
1261110 0.922 0. 1. 1.
1262110 1.289 0. 1. 1.
*

```

```

*rcdcp
* the following data connection between the uh and core *
* and represents the rcc flow path
*

```

```

*crdno component name component type
1290000 rccfp branch
*
*crdno number of junctions vel/flw
1290001 2 0
*
*crdno flow area length volume
1290101 0.0 10.922 10.9220
*
*crdno horz orient vert orient delta z
1290102 0.0 90.0 10.922
*
*crdno roughness hyd. diameter fe
1290103 0.00015 0.0 00
*

```

```

*crdno vol ic pressure eq temp
1290200 0 2264.4000 611.25000 1051.2000 .00000000
*
*crdno from to area f loss r loss cabs
1291101 129010000 129010000 0.0 1.5650 1.5650 0000
1292101 129010000 129000000 0.0 1.5650 1.5650 0000
*
*crdno f flowrate g flowrate j flowrate
1291201 7.4024000 7.4024000 0.0
1292201 7.423000 7.4023000 0.0
*
* crdno jun dia beta c m
1291110 1.128 0. 1. 1.
1292110 1.128 0. 1. 1.
*

```

```

$loop a - includes the hot leg, steam generator inlet plenum, u-tubes, $
$steam generator outlet plenum, pump suction leg, rc pump, and cold leg $
$loop a hot leg $

```

```

*hydro component name component type
2040000 'hotleg1' pipe
*
*hydro no. volumes
2040001 4
*
*hydro vol area
2040101 0. 4
*
*hydro jun area
2040201 0. 3
*
*hydro length
2040301 6.3105 3
2040302 6.7932 4
*
*hydro volume
2040401 24.4874 1
2040402 24.3590 3
2040403 33.1338 4
*
*hydro vert angle
2040601 0. 3
2040602 26.19 4
*
*hydro delta z
2040701 0. 3
2040702 3.0998 4
*
*hydro roughness hyd dia
2040901 0.00015 0. 4
*
*hydro f loss r loss
2040902 0. 0 2
2040902 05 05 3
*
*hydro fe
2041001 0 4
*
*hydro frcabs
2041101 000000 3
*
*hydro ic pressure eq temp
2041201 0 2249.2000 610.49000 1052.300 00000000 0.0 21

```

```

2041202 0 2248.8000 610.50000 1052.3000 .00000000 0.0 02
2041203 0 2248.6000 610.50000 1052.4000 .00000000 0.0 03
2041204 0 2248.9000 610.50000 1052.3000 .00000000 0.0 04

```

```

*hydro vel/flw
2041300 0
*
*hydro f flowrate g flowrate j flowrate jun
2041301 47.696000 47.696000 0.0 01
2041302 47.697000 47.697000 0.0 02
2041303 47.697000 47.697000 0.0 03
*
* junc dia beta c m
2041401 2.417 0. 1. 1. 3

```

```

$loop a steam generator inlet plenum
$

```

```

*hydro component name component type
2060000 'sg inlet' branch
*-----*
*hydro no. junc vel/flw
2060001 2 0
*
*hydro area length volume
2060101 0 3.28 115.1
*
*hydro horz angle vert angle delta z
2060102 0. 90. 3.28
*
*hydro roughness hyd diam fe
2060103 0.00015 0. 80

```

```

2060200 0 2250.2000 610.50000 1052.2000 .00000000

```

```

*hydro from to area f loss r loss vcahs
2061101 204010000 206000000 0.0 0. 0. 00100
2062101 206010000 206000000 10.53 0. 0. 00100
*
2061201 44.855000 44.855000 0.0
2062201 20.777000 20.777000 0.0
*
* junc dia beta c m
2061110 2.492 0. 1. 1.
2062110 0.06458 0. 1. 1.

```

```

$loop a u-tubes
$

```

```

*hydro component name component type
2080000 'sg tubes' pipe
*-----*
*hydro no. volumes
2080001 8
*
*hydro vol area vol
2080101 10.53 8
*
*hydro length vol
2080201 7.834 8
*
*hydro volume vol
2080401 0.0 8
*
*hydro vert angle vol
2080601 90. 4

```

```

2080602 -90. 8
*
*hydro roughness hyd diam vol
2080801 0.00015 0.06458 8
*
*hydro fe vol
2081001 80 8
*
*hydro fvcchs jun
2081101 0.00000 7

```

```

2081201 0 2242.9000 595.99000 1052.8000 .00000000 0.0 01
2081202 0 2234.7000 581.09000 1053.3000 .00000000 0.0 02
2081203 0 2226.7000 579.21000 1053.9000 .00000000 0.0 03
2081204 0 2218.6000 559.75000 1054.5000 .00000000 0.0 04
2081205 0 2213.2000 551.68000 1054.9000 .00000000 0.0 05
2081206 0 2210.2000 544.44000 1055.1000 .00000000 0.0 06
2081207 0 2207.4000 538.10000 1055.3000 .00000000 0.0 07
2081208 0 2204.8000 533.60000 1055.5000 .00000000 0.0 08
2081300 0
*
2081301 20.351000 20.351000 0.0 01
2081302 19.955000 19.955000 0.0 02
2081303 19.654000 19.654000 0.0 03
2081304 19.432000 19.432000 0.0 04
2081305 19.248000 19.248000 0.0 05
2081306 19.086000 19.086000 0.0 06
2081307 18.952000 18.952000 0.0 07
*
* junc dia beta c m
2081401 0.06458 0. 1. 1. 7

```

```

$loop a steam generator outlet plenum
$

```

```

*hydro component name component type
2100000 'sg outle' branch
*-----*
*hydro no. junc vel/flw
2100001 2 0
*
*hydro area length volume
2100101 0.0 3.28 115.1
*
*hydro horz angle vert angle delta z
2100102 0.0 -90. -3.28
*
*hydro roughness hyd diam fe
2100103 0.00015 0.0 80

```

```

2100200 0 2204.3000 533.61000 1055.5000 .00000000

```

```

*hydro from to area f loss r loss vcahs
2101101 210010000 212000000 4.9 0. 0.0 00100
2102101 208010000 210000000 10.53 0.0 0.0 00100
*
2101301 35.945000 35.945000 0.0
2102201 18.858000 18.858000 0.0
*
* junc dia beta c m
2101110 2.498 0. 1. 1.
2102110 0.06458 0. 1. 1.

```

```

$loop a pump suction leg
$

```

```

*hydro component name component type

```

```

2120000      'rcaustic'      pipe
-----
*hydro      no. volumes
2120001      5
*
*hydro      vol area      vol
2120101      0.      5
*
*hydro      jun area      jun
2120201      0.      4
*
*hydro      length      vel
2120301      4.9599      1
2120302      2.7219      2
2120303      7.1209      3
2120304      4.2250      4
2120305      7.1209      5
*
*hydro      volume      vol
2120401      27.4002      1
2120402      14.2667      2
2120403      37.3240      3
2120404      22.1461      4
2120405      37.3240      5
*
*hydro      vert angle      vel
2120601      -80.      1
2120602      -90.      2
2120603      -39.54      3
2120604      0.      4
2120605      39.54      5
*
*hydro      delta z      vel
2120701      -4.2952      1
2120702      2.7219      2
2120703      -4.5333      3
2120704      0.      4
2120705      4.5333      5
*
*hydro      roughness      hyd diam      vel
2120801      .00015      0.      5
*
*hydro      f loss      r loss      jun
2120901      .053      .053      1
2120902      0.      0.      2
2120903      .1      .1      3
2120904      .1      .1      4
*
*hydro      fe      vel
2121001      0      5
*
*hydro      fvchs      jun
2121101      000000      4
*
*hydro      ic      pressure      eq. temp      vol
2121201      0      2194.8000      533.61000      1056.2000      .00000000      0.0      01
2121202      0      2194.9000      533.61000      1056.2000      .00000000      0.0      02
2121203      0      2196.0000      533.61000      1056.1000      .00000000      0.0      03
2121204      0      2195.8000      533.61000      1056.1000      .00000000      0.0      04
2121205      0      2194.2000      533.61000      1056.2000      .00000000      0.0      05
*
*hydro      vel/flw
2121300      0

```

```

*
*hydro      f flowrate      g flowrate      j flowrate      jun
2121301      37.889000      37.889000      0.0      01
2121302      37.888000      37.888000      0.0      02
2121303      37.888000      37.888000      0.0      03
2121304      37.888000      37.888000      0.0      04
*
*hydro      junc dia      beta      c      a      d
2121401      2.583      0.      1.      1.      4
$loop a reactor coolant pump

```

```

-----
*hydro      component name      component type
2140000      'a rcp'      pump
-----
*hydro      area      length      volume
2140101      0.0      4.0083      183.7506
*
*hydro      horz angle      vert angle      delta z
2140102      0      90.0      4.0083
*
*hydro      equil flag
2140103      0
*
*hydro      from      jun area      f loss      r loss      fvchs
2140108      21201000      5.2414      0.0      0.0      00000
*
*hydro      to      jun area      f loss      r loss      fvchs
2140109      216000000      4.1247      0.0      0.0      00000
*
*hydro      junc dia      beta      c      a
2140110      2.583      0.      1.      1.
2140111      2.292      0.      1.      1.
*
*hydro      ic      pressure      eq. temp
2140200      0      2250.5000      533.69000      1052.2000      .00000000
*
*hydro      vel/flw      f flowrate      g flowrate      j flowrate
2140201      0      37.889000      37.889000      0.0
2140202      0      48.128000      48.128000      0.0
$loop b reactor coolant pump
-----
*hydro      ptdi      2fazi      diff i      fork i      pvel i      trip no.      rvrs i
2140301      0      0      -2      -1      0      523      0
2140302      1190.0000      1.0432775      88500.000      277.00000      23900.000      70000.000
2140303      47.180000      .00000000      .00000000      239.00000      23.900000      .00000000
*
*hydro      rated pump vel.      init/rated vel.      rated flow      rated head
*
*hydro      rated torque      mom of inertia      rated dens      str torque
*
*hydro      coeff. if2      coeff. if3      coeff. if1      coeff. if0
*
*hydro      curve type      regime
2141100      1      1
*
*hydro      v/a      head      inchoal      (ft,m)
2141101      0.000      1.747
2141102      0.042      1.714
2141103      0.037      1.692
2141104      0.150      1.643
2141105      0.196      1.597
2141106      0.253      1.640
2141107      0.299      1.481
2141108      0.35      1.414
2141109      0.506      1.368
2141110      0.451      1.326

```



2141111	0.497	1.304
2141112	0.546	1.280
2141113	0.593	1.265
2141114	0.640	1.250
2141115	0.670	1.255
2141116	0.692	1.261
2141117	0.715	1.261
2141118	0.738	1.253
2141119	0.773	1.238
2141120	0.792	1.219
2141121	0.824	1.197
2141122	0.852	1.170
2141123	0.878	1.139
2141124	0.914	1.098
2141125	0.947	1.055
2141126	0.974	1.017
2141127	1.000	1.000

*hydro	curve type	regime		
2141200	1	2		
*hydro	a/v	head	\$normal	(+q, +h)
2141201	0.000	-1.554		
2141202	0.197	-1.104		
2141203	0.397	-0.641		
2141204	0.499	-0.411		
2141205	0.598	-0.152		
2141206	0.657	0.001		
2141207	0.698	0.102		
2141208	0.762	0.240		
2141209	0.843	0.490		
2141210	0.895	0.648		
2141211	0.944	0.808		
2141212	0.978	0.923		
2141213	0.999	0.985		
2141214	1.000	1.000		

*hydro	curve type	regime		
2141300	1	3		
*hydro	v/a	head	\$dissipation (-q, +h)	
2141301	-1.000	4.224		
2141302	-0.799	3.500		
2141303	-0.597	2.993		
2141304	-0.398	2.483		
2141305	-0.201	2.061		
2141306	-0.078	1.639		
2141307	-0.023	1.765		
2141308	0.000	1.747		
*hydro	curve type	regime		
2141400	1	4		
*hydro	a/v	head	\$dissipation (-q, +h)	
2141401	-1.000	4.224		
2141402	-0.799	3.542		
2141403	-0.590	2.822		
2141404	-0.399	2.395		
2141405	-0.203	2.171		
2141406	-0.222	1.996		
2141407	-0.172	1.918		
2141408	-0.150	1.850		
2141409	-0.096	1.754		

2141410	0.044	1.685		
2141411	0.000	1.626		
*hydro	curve type	regime		
2141500	1	5		
*hydro	v/a	torque	\$dissipation (-q, +h)	
2141501	0.000	1.000		
2141502	1.000	2.000		
*hydro	curve type	regime		
2141600	1	6		
*hydro	v/a	torque	\$dissipation (-q, +h)	
2141601	0.000	1.636		
2141602	1.000	2.000		
*hydro	curve type	regime		
2141700	1	7		
*hydro	v/a	torque	\$dissipation (-q, +h)	
2141701	-1.000	0.200		
2141702	0.000	1.000		
*hydro	curve type	regime		
2141800	1	8		
*hydro	v/a	torque	\$dissipation (-q, +h)	
2141801	-1.000	0.200		
2141802	0.000	1.524		
*hydro	curve type	regime		
2141900	2	1		
*hydro	v/a	torque	\$normal	(+q, +h)
2141901	0.000	0.044		
2141902	0.037	0.049		
2141903	0.076	0.054		
2141904	0.151	0.062		
2141905	0.199	0.063		
2141906	0.239	0.057		
2141907	0.262	0.058		
2141908	0.294	0.054		
2141909	0.341	0.043		
2141910	0.387	0.050		
2141911	0.455	0.054		
2141912	0.525	0.050		
2141913	0.579	0.068		
2141914	0.622	0.077		
2141915	0.681	0.094		
2141916	0.732	1.008		
2141917	0.767	1.017		
2141918	0.805	1.025		
2141919	0.862	1.024		
2141920	0.904	1.019		
2141921	1.000	1.000		

*hydro	curve type	regime		
2142000	2	2		
*hydro	a/v	torque	\$normal	(+q, +h)
2142001	0.000	-1.475		
2142002	0.127	-1.079		
2142003	0.198	-0.882		





```

2580401      150.5      1
*
*hydro      vert angle      vol
2580601      90.      1
*
*hydro      roughness      hyd diam      vol
2580801      0.00015      2.58      1
*
*hydro      fe      vol
2581001      00      1
*
2581201  0      807.97000 491.68000 1114.9000 08818765 0.0      01
*
*****
*hydro      component name      component type
2600000      'feed jun'      sngljun
*****
*hydro      from      to      area      f loss      r loss      fvcabs
2600101  258010000      262000000      0.      2.0      3.0      030100
*
2600201  0      5.6658000 5.1485000 0.0
*
*hydro      junc dia      beta      c      s
2600110  1.24      0.      1      1
*****
*hydro      component name      component type
2620000      'downcase'      annulus
*****
*hydro      no. volumes
2620001      4
*
*hydro      vol area      vol
2620101      17.94      1
2620102      5.609      4
*
*hydro      length      vol
2620301      7.834      3
2620302      6.016      4
*
*hydro      volume      vol
2620401      0.      4
*
*hydro      vert angle      vol
2620601      90.      4
*
*hydro      roughness      hyd diam      vol
2620801      0.00015      1.24      1
2620802      0.00015      0.362      4
*
*hydro      fe      vol
2621001      00      4
*
*hydro      vcats      jun
2621101      01100      1
2621102      01000      3
*
2621201  0      809.48700 492.59000 1114.9000 09483950 0.0      01
2621202  0      810.11200 492.68000 1114.9000 02651870 0.0      02
2621203  0      812.21000 493.13000 1114.9000 02040390 0.0      03
2621204  0      814.04000 493.28000 1114.9000 01448350 0.0      04
2621300  0
*
2621301  17.347000 16.185000 0.0      01
2621302  17.208000 16.357000 0.0      02

```

```

2621303  17.109000 16.281000 0.0      03
*
*hydro      junc dia      beta      c      s
2621401  0.362      0.      1      1      3
*****
*hydro      component name      component type
2640000      'dc to bc'      sngljun
*****
*hydro      from      to      area      f loss      r loss      fvcabs
2640101  262010000      266000000      0.0      2.4      2.4      030100
*
2640101  0      17.010000 19.066000 0.0
*
*hydro      junc dia      beta      c      s
2640110  0.126      0.      1      1
*****
*hydro      component name      component type
2660000      'sg boiler'      pipe
*****
*hydro      no. volumes
2660001      4
*
*hydro      vol area      vol
2660101      0.0      4
*
*hydro      length      vol
2660301      6.016      1
2660302      7.834      4
*
*hydro      volume      vol
2660401      281.2      1
2660402      267.0      2
2660403      359.4      3
2660404      283.8      4
*
*hydro      vert angle      vol
2660601      90.      4
*
*hydro      roughness      hyd diam      vol
2660801      0.00015      0.126      4
*
*hydro      f loss      r loss      jun
2660901      12.0      12.0      1
2661002      9.0      9.0      3
*
*hydro      fe      vol
2661001      100      4
*
*hydro      fvcabs      jun
2661101      000000      3
*
2661201  0      812.33000 508.29000 1114.9000 7804000 0.0      01
2661202  0      810.60000 508.56000 1114.9000 8757000 0.0      02
2661203  0      808.83000 508.29000 1115.1000 70582000 0.0      03
2661204  0      807.29000 508.91000 1115.3000 85331000 0.0      04
2661300  0
*
2661301  3.1947000 5.2341000 0.0      01
2661302  5.0996000 8.5578000 0.0      02
2661303  8.5509000 11.645000 0.0      03
*
*hydro      junc dia      beta      c      s
2661401  0.016      0.      1      1      3 *Hyd Diam. of tube supp. pl.
*****
*hydro      component name      component type
2680000      'abv boiler'      sngljun

```

```

*hydro from to area f loss r loss vcahs
2660101 266010000 270000000 0.0 0.0 0.0 030000
*
2660201 0 10.646000 12.956000 0.0
*
2660110 0 0.128 0 1 1
*
*-----*
*hydro component name component type
2700000 "above lu" anglvol
*-----*
*hydro area length volume
2700101 0.0 4.405 263.5
*
*hydro horz angle vert angle delta z
2700102 0.0 90 4.405
*
*hydro roughness hyd diam fe
2700103 0.00015 10.53 00
*
2700200 0 806.79000 507.82000 1115.4000 85406000
*
*hydro component name component type
2720000 "abv tube" singjun
*-----*
*hydro from to area f loss r loss vcahs
2720101 270010000 274000000 0.0 0.0 0.0 030000
*
2720201 0 8.2555000 9.9979000 0.0
*
2720110 0 5.190 0 1 1
*
*-----*
*hydro component name component type
2740000 "below be" anglvol
*-----*
*hydro area length volume
2740101 0.0 7.88 500.44
*
*hydro horz angle vert angle delta z
2740102 0.0 90 7.88
*
*hydro roughness hyd diam fe
2740103 0.00015 6.19 00
*
2740200 0 806.41000 507.86000 1115.1000 87642000
*
*hydro component name component type
2780000 "separato" separatr
*-----*
*hydro no. juns vel/ft
2780001 3 0
*
*hydro area length volume
2780101 0.0 5.29 697.2
*
*hydro horz angle vert angle delta z
2780102 0.0 90.0 5.29
*
*hydro roughness hyd diam fe
2780103 0.00015 0.17 00
*
2780200 0 806.54000 507.71000 1115.0000 18072000

```

```

*hydro from to area f loss r loss vcahs
2781101 278010000 282000000 0.0 127.5 127.5 01300 0.02
2782101 278000000 284000000 0.0 90.0 90.0 01000 1.6
2787101 274010000 278000000 6.3 0.0 0.0 01036
*
2781201 4.7025000 4.8133000 0.0
2782201 1.3416000 1.1743000 0.0
2783201 9.7460000 9.7460000 0.0
*
*hydro junc dia beta c w
2781110 1.0 0. 1. 1.
2782110 2.59 0. 1. 1.
2783110 1.0 0. 1. 1.
*
*hydro component name component type
2820000 "steep do" branch
*-----*
*hydro no. juns vel/ft
2820001 1 0
*
*hydro area length volume
2820101 0.0 6.32 696.3
*
*hydro horz angle vert angle delta z
2820102 0.0 50 6.32
*
*hydro roughness hyd diam fe
2820103 0.00015 8.187 00
*
2820200 0 804.28000 507.48000 1114.8800 1.0360000
*
*hydro from to area f loss r loss vcahs
2821101 282010000 286000000 1.38 1.5 1.5 60000
*
2821201 380.12000 380.67000 0.0
*
*hydro junc dia beta c w
2821110 0.087 0. 1. 1.
*
*-----*
*loop b - includes the hot leg, steam generator inlet plenum, u-tubes,
*steam generator outlet plenum, loop suction leg, dc pump, pressurizer,
*surge line, pressurizer, spray line, psv, and safety valves
*-----*
*loop b hot leg
*
*hydro component name component type
3040000 "hot leg" pipe
*-----*
*hydro no. volumes
3040001 4
*
*hydro vol area
3040101 0
*
*hydro length
3040201 6 1.05
3040301 6 7932
*
*hydro volume
3040401 24 4075
3040402 24 9530
3040403 24 1188

```



```

*
*hydro      vert angle      vol
3040601    0                    3
3040602    26.29                 4
*
*hydro      delta z          vol
3040701    0                    3
3040702    3.0088                4
*
*hydro      roughness      hyd diam      vol
3040801    .00015                0.                    4
*
*hydro      f loss          r loss          jun
3040901    0                    0.                    2
3040902    .65                  .05                  3
*
*hydro      fe                    vol
3041001    0                    4
*
*hydro      frcchs          jun
3041101    000000                3
*
*hydro      pressure      eq. temp      vol
3041201    0                    2249.2000 610.49000 1052.3000 00000000 0.0 01
3041202    0                    2248.8000 610.50000 1052.3000 00000000 0.0 02
3041203    0                    2248.6000 610.50000 1052.4000 00000000 0.0 03
3041204    0                    2248.9000 610.49000 1052.3000 00000000 0.0 04
*
*hydro      vel/flw          vol
3041300    0
*
*hydro      f flowrate      g flowrate      j flowrate      jun
3041301    47.711000 47.711000 0.0 01
3041302    47.711000 47.711000 0.0 02
3041303    47.712000 47.712000 0.0 03
*
*hydro      junc dia      beta      c      m
3041401    2.417          0.        1.        1.        3
*
*****
$loop b steam generator inlet plenum
$
*hydro      component name      component type
3060000      'sg inlet'            branch
*
*hydro      no. junc          vel/flw
3060001    2                    0
*
*hydro      area          length          volume
3060101    0.                3.28            115.1
*
*hydro      horz angle      vert angle      delta z
3060102    0.                90.             3.28
*
*hydro      roughness      hyd diam      fe
3060103    .00015          0.
*
*hydro      3060200    0                    2250.2000 610.50000 1052.2000 00000000
*
*hydro      from          to          area      f loss      r loss      vcrchs
3061101    304010000    306000000    0.0      0.          0.          00100
3062101    306010000    308000000    10.53    0.          0.          00100
*

```

```

3061201    44.869000 44.869000 0.0
3062201    20.783000 20.783000 0.0
*
*hydro      junc dia      beta      c      m
3061110    2.452          0.        1.        1.
3062110    0.06458        0.        1.        1.
*
*****
$loop b steam generator u-tubes
$
*hydro      component name      component type
3080000      'sg tubes'            pipe
*
*hydro      no. volumes
3080001    8
*
*hydro      vol area          vol
3080101    10.53                8
*
*hydro      length          vol
3080301    7.834                8
*
*hydro      volume          vol
3080401    0.0                  8
*
*hydro      vert angle      vol
3080601    90.                  4
3080602    -90.                 8
*
*hydro      roughness      hyd diam      vol
3080801    0.00015          .06458        8
*
*hydro      fe                    vol
3081001    00                8
*
*hydro      frcchs          jun
3081101    000000                7
*
3081201    0                    2242.9000 595.94000 1052.8000 00000000 0.0 01
3081202    0                    2234.7000 595.99000 1052.3000 00000000 0.0 02
3081203    0                    2226.6000 599.07000 1052.9000 00000000 0.0 03
3081204    0                    2218.6000 559.57000 1054.5000 00000000 0.0 04
3081205    0                    2213.1000 561.47000 1054.9000 00000000 0.0 05
3081206    0                    2210.2000 644.21000 1055.1000 00000000 0.0 06
3081207    0                    2207.8000 537.85000 1055.3000 00000000 0.0 07
3081208    0                    2204.5000 523.33000 1055.5000 00000000 0.0 08
3081300    0
*
3081301    20.356000 20.356000 0.0 01
3081302    19.956000 19.956000 0.0 02
3081303    19.657000 19.657000 0.0 03
3081304    19.434000 19.434000 0.0 04
3081305    19.247000 19.247000 0.0 05
3081306    19.087000 19.087000 0.0 06
3081307    18.952000 18.952000 0.0 07
*
*hydro      junc dia      beta      c      m
3081401    0.06458        0.        1.        1.        7
*
*****
$loop b steam generator outlet plenum
$
*hydro      component name      component type
3100000      'sg outlet'           branch
*
*hydro      no. junc          vel/flw
3100001    2                    0
*

```

```

*hydro      area      length      volume
3100101    0.0          3.26        116.1
*
*hydro      horz angle  vert angle  delta z
3100102    0.0          -90         -3.26
*
*hydro      roughness   hyd diam    fe
3100103    0.0015      3.0         00
*
3100206    0          2204.3000  533.34000  1056.5000  00000000
*
*hydro      from      to          area      f loss    r loss    vcats
3101101    310010000  312000000  4.9       0.0       0.0       00100
3102101    306010000  310000000  10.52     0.0       0.0       00100
*
*
3101201    35.9460000  35.9460000  0.0
3102201    18.8580000  18.8580000  0.0
*
*hydro      junc dia  beta      c      m
3101110    2.498     0.        1.      1.
3102110    0.06458  0.        1.      1.
*
*****
$loop b pump suction leg
$
*hydro      component name  component type
3120000      'suction'        pipe
*
*hydro      no. volumes
3120001      5
*
*hydro      vol area      vol
3120101      0.            5
*
*hydro      length      vol
3120301      4.9599       1
3120302      2.7219       2
3120303      7.1109       3
3120304      4.2250       4
3120305      7.1206       5
*
*hydro      volume      vol
3120401      37.3402      1
3120402      14.2667     2
3120403      37.3240     3
3120404      22.1451     4
3120405      37.3240     5
*
*hydro      vert angle  vol
3120601      -66.         1
3120602      -90.         2
3120603      -39.54      3
3120604      0.          4
3120605      39.54      5
*
*hydro      delta z     vol
3120701      -4.2952     1
3120702      -2.7219     2
3120703      -4.5333     3
3120704      0.          4
3120705      4.5333     5
*
*hydro      roughness   hyd diam    vol
3120801      0.0015      0.          5

```

```

*
*hydro      f loss      r loss      jun
3120901      .053        .053        1
3120902      0.          0.          2
3120903      .1          .1          4
*
*hydro      fe          vol
3121001      0           5
*
*hydro      fvcats     jun
3121101      000000     4
*
*hydro      ic      pressure    eq. temp    vol
3121201    0        2194.8000  533.34000  1056.2000  00000000  0.0  01
3121202    0        2194.8000  533.34000  1056.2000  00000000  0.0  02
3121203    0        2196.0000  533.34000  1056.1000  00000000  0.0  03
3121204    0        2195.8000  533.34000  1056.1000  00000000  0.0  04
3121205    0        2194.1000  533.34000  1056.2000  00000000  0.0  05
*
*hydro      vel/flw
3121300    0
*
*hydro      f flowrate  g flowrate  j flowrate  jun
3121301    37.8890000  37.8890000  0.0         01
3121302    37.8890000  37.8890000  0.0         02
3121303    37.8890000  37.8890000  0.0         03
3121304    37.8890000  37.8890000  0.0         04
*
*hydro      junc dia  beta      c      m
3121401    2.583     0.        1.      4
*
*****
$loop b reactor coolant pump
$
*hydro      component name  component type
3140000      'b rcp'        pump
*
*hydro      area      length      volume
3140101    0.0       4.0093      183.7506
*
*hydro      horz angle  vert angle  delta z
3140102    0         90.0       4.0093
*
*hydro      equi flag
3140103    0
*
*hydro      from      jun area    f loss    r loss    vcats
3140108    312010000  5.2414     0.0       0.0       00000
*
*hydro      to        jun area    f loss    r loss    vcats
3140109    312000000  4.1247     0.0       0.0       00000
*
*hydro      junc dia  beta      c      m
3140110    2.583     0.        1.      1.
3140111    2.292     0.        1.      1.
*
*hydro      ic      pressure    eq. temp
3140200    0        2250.5000  533.42000  1112.2500  00000000
*
*hydro      vel/flw    f flowrate  g flowrate  j flowrate
3140201    0          37.8890000  37.8890000  0.0
3140202    0          45.1290000  48.1290000  0.0
*
*****
*hydro      ptds  2fazi  diff  i  tork  j  pvel  i  trip nu.  rvrs  i
3140301    214  214  2  -1  214  523  0
3140302    1190 0000 1.6432773 89500 800 277 00000 22900 000 79000 800
3140303    47.180000 00000000 00000000 239.00000 23 000000 00000000

```

```

*hydro rated pump vel. 30.11/rated vel. rated flow rated head
*hydro rated torque Mom of inertia rated dens str torque
*hydro coeff. 1f1 coeff. 1f0 coeff. 1f1 coeff. 1f3
*
*****
loop & pump discharge and cold leg
*
*hydro component name component type
3180000 "pumpdis2" engivol
*
*hydro area length volume
3180101 4.1247 3.4292 0.
*
*hydro horz angle vert angle delta z
3180102 0. 0. 0.
*
*hydro roughness hyd diam fe
3180103 .00015 0. 00
*
*hydro ic pressure eq temp
3180200 0 2288.9820 533.42000 1048.5000 00000000
*
*****
*hydro component name component type
3180000 "pumpdis2" branch
*
*hydro no. juns vel/flw
3180001 4 0
*
*hydro area length volume
3180101 4.1247 3.4594 0.
*
*hydro horz angle vert angle delta z
3180102 0. 0. 0.
*
*hydro roughness hyd diam fe
3180103 .00015 0. 00
*
*hydro ic pressure eq temp
3180200 0 2288.3000 533.42000 1048.8000 00000000
*
*hydro from to area f loss r loss vcrhs
3181101 318010000 318000000 4.1247 0. 0. 00000
3182101 318010000 320110000 4.1247 0. 0. 00000
3183101 320110000 318000000 .3941 0. 0. 00100
3184101 318000000 325000000 .0640 0. 0. 00100
*
*hydro f flowrate g flowrate j flowrate
3181201 48.110000 48.110000 0.0
3182201 48.110000 48.110000 0.0
3183201 .0077800 .0077800 0.0
3184201 .209001-3 .209001-3 0.0
*
*hydro junc dia beta c m
3181110 2.292 0. 1. 1.
3182110 2.292 0. 1. 1.
3183110 0.0 0. 1. 1.
*
*****
*hydro component name component type
3200000 "pumpdis2" pipe
*
*hydro vol volume

```

```

3200001 2
*
*hydro vol area vol
3200101 0.
*
*hydro junc area junc
3200201 4.1247
*
*hydro length vol
3200301 3.4594 1.
3200302 3.4594 2.
*
*hydro volume vol
3200401 22.5140 1.
3200402 26.4377 2.
*
*hydro vert angle vol
3200001 0. 2.
*
*hydro delta z vol
3200001 0. 2.
*
*hydro roughness hyd diam vol
3200001 .00015 0. 2.
*
*hydro f loss r loss junc
3200001 .029 .029 1.
*
*hydro fe vol
3200001 0. 2.
*
*hydro fvcans junc
3200001 000000
*
*hydro ic pressure eq temp vol
3201201 0 2288.4000 533.42000 1048.8000 00000000 0.0 01
3201202 0 2291.8000 533.42000 1048.3000 00000000 0.0 02
*
*hydro vol/flw
3201300 0
*
*hydro f flowrate g flowrate j flowrate junc
3201301 48.110000 48.110000 0.0 01
3201401 2.292 0. 1. 1. 1.

```

```

*****
The following input represents the pressurizer system including the
surge and spray lines, and the pop and vade safety valves, the surge
line is connected to the loop c hot leg.
*
*hydro component name component type
3250000 "spraylin" engivol
*
*hydro area length volume
3250101 0.648 42.520 0.
*
*hydro horz angle vert angle delta z
3250102 0. 0. 30.178
*
*hydro roughness hyd diam fe
3250103 .00015 0. 00
*
*hydro ic pressure eq temp

```

```

0350200 0 215.9000 530 23000 1048 2000 00000000
*****
*hydro component name component type
0360000 'spraylx' valve
*
*hydro from to area f loss r loss vchgs
0360101 235010000 239000000 .0645 9.245 9.245 00100
*
*hydro i/wc dia beta c a
0360110 0.0 0. 1. 1.
*
*hydro vel/flw f flowrate g flowrate j flowrate
0360201 0 .00000000 .00000000 0.0
*
*hydro valve type
0360300 'spraylv'
*
*hydro driver table no.
0360301 213
*****
*hydro component name component type
0370000 'spraylin' angvol
*
*hydro area length volume
0370101 .0645 80.2178 0.
*
*hydro horz angle vert angle delta 1
0370102 0. 90.0 96.276
*
*hydro roughness hyd diam fe
0370103 .00015 0. 60
*
*hydro ic pressure eq temp
0370200 0 2251.8000 534.42000 1048 2000 00000000
*****
*hydro component name component type
0380000 'spraylv' valve
*
*hydro from to area f loss r loss vchgs
0380101 037010000 339000000 .0640 9.245 9.245 00100
*
*hydro i/wc dia beta c a
0380110 0.0 0. 1. 1.
*
*hydro vel/flw f flowrate g flowrate j flowrate
0380201 0 .00000000 .00000000 0.0
*
*hydro valve type
0380300 'spraylv'
*
*hydro driver table no.
0380301 213
*****
*hydro component name component type
0390000 'spraylin' branch
*
*hydro no. joints vel/flw
0390001 0 1
*
*hydro area length volume
0390101 .0645 28.2031 0.
*
*hydro horz angle vert angle delta 2
0390102 0. 90.0 9.0
*
*hydro roughness hyd diam fe
0390103 .00015 0. 60
*
*hydro ic pressure eq temp
0390200 0 2251.5000 544.84000 1052 2000 00000000
*****
*hydro component name component type
0400000 'prztrac' branch
*
*hydro no. joints vel/flw
0400001 2 0
*
*hydro area length volume
0400101 0. 3.5 89.7972
*
*hydro horz angle vert angle delta 2
0400102 0. -90. -3.5
*
*hydro roughness hyd diam fe
0400103 .00015 0. 60
*
*hydro ic pressure quality
0400200 0 2250.1000 590.11000 1051.0000 1.00000000
*
*hydro from to area f loss r loss vchgs
0400101 339010000 340000000 .0645 5.14 0.14 00000
*
*hydro from to area f loss r loss vchgs
0400101 340010000 341000000 38.4845 0. 0. 00000
*
*hydro f flowrate g flowrate j flowrate
0400201 5 582400 17.88000 0.0
*
*hydro f flowrate g flowrate j flowrate
0400201 15770000 453642 4 0.0
*****
*hydro component name component type
0410000 'prz' pipe
*
*hydro no. volumes
0410001 7
*
*hydro vol area vol
0410101 0. 7
*
*hydro jun area jun
0410201 38.4845 6
*
*hydro length vol
0410301 4.8022 6
*
*hydro length vol
0410302 0.5 7
*
*hydro volume vol
0410401 185.7543 6
*
*hydro volume vol
0410402 89.7972 7
*
*hydro vert angle vol
0410501 -90. 7
*
*hydro roughness hyd diam vol
0410601 .00015 0. 7
*
*hydro fr vol
0410701 7

```

```

*hydro roughness hyd diam fe
0390103 .00015 0. 60
*
*hydro ic pressure eq temp
0390200 0 2251.5000 544.84000 1052 2000 00000000
*****
*hydro component name component type
0400000 'prztrac' branch
*
*hydro no. joints vel/flw
0400001 2 0
*
*hydro area length volume
0400101 0. 3.5 89.7972
*
*hydro horz angle vert angle delta 2
0400102 0. -90. -3.5
*
*hydro roughness hyd diam fe
0400103 .00015 0. 60
*
*hydro ic pressure quality
0400200 0 2250.1000 590.11000 1051.0000 1.00000000
*
*hydro from to area f loss r loss vchgs
0400101 339010000 340000000 .0645 5.14 0.14 00000
*
*hydro from to area f loss r loss vchgs
0400101 340010000 341000000 38.4845 0. 0. 00000
*
*hydro f flowrate g flowrate j flowrate
0400201 5 582400 17.88000 0.0
*
*hydro f flowrate g flowrate j flowrate
0400201 15770000 453642 4 0.0
*****
*hydro component name component type
0410000 'prz' pipe
*
*hydro no. volumes
0410001 7
*
*hydro vol area vol
0410101 0. 7
*
*hydro jun area jun
0410201 38.4845 6
*
*hydro length vol
0410301 4.8022 6
*
*hydro length vol
0410302 0.5 7
*
*hydro volume vol
0410401 185.7543 6
*
*hydro volume vol
0410402 89.7972 7
*
*hydro vert angle vol
0410501 -90. 7
*
*hydro roughness hyd diam vol
0410601 .00015 0. 7
*
*hydro fr vol
0410701 7

```

```

3411001      0      7
*
*hydro      fvcahs      jun
3411101      000000      6
*
*hydro      ic      pressure      quality      vol
3411201      0      2250.0000      690.21000      1052.0000      1.00000000      0.0      01
3411202      0      2250.0000      690.23000      1052.0000      1.00000000      0.0      02
3411203      0      2250.0000      690.26000      1052.0000      1.00000000      0.0      03
3411204      0      2251.0000      690.02000      1052.0000      1.00000000      0.0      04
3411205      0      2252.0000      690.41000      1052.0000      1.00000000      0.0      05
3411206      0      2254.0000      685.58000      1052.0000      1.00000000      0.0      06
3411207      0      2255.0000      688.69000      1051.0000      1.00000000      0.0      07
*

```

```

*hydro      vel/flw
3411300      0
*
*hydro      f flowrate      g flowrate      j flowrate      jun
3411301      14159000      269186      0.0      01
3411302      24.112000      441896      3.0      02
3411303      00797751      30.83100      0.0      03
3411304      723526      3      242000      0.0      04
3411305      732000      3      2582100      0.0      05
3411306      743294      3      1751100      0.0      06
*
*      unc dia      beta      c      m
3411401      7.000      0.      1.      1.      6

```

```

*hydro      component name      component type
3420000      'surgein1'      engljun
*-----*
*hydro      from      to      area      f loss      r loss      fvcahs
3420101      341010000      343000000      7213      .472      .985      030000
*
*      unc dia      beta      c      m
3420110      0.875      0.      1.      1.

```

```

*hydro      vel/flw      f flowrate      g flowrate      j flowrate
3420201      0      03974050      -0.048737      0.0
*-----*
*hydro      component name      component type
3430000      'surgein1'      pipe

```

```

*hydro      no. volumes
3430001      3
*
*hydro      vol area      vol
3430101      0.      3
*
*hydro      jun area      jun
3430201      6013      2
*
*hydro      length      vol
3430301      12.5549      1
3430302      22.3757      2
3430303      23.0502      3
*
*hydro      volume      vol
3430401      7.8899      1
3430402      13.4545      2
3430403      13.9601      3
*
*hydro      vert angle      vol
3430501      -46.87      1
3430502      0.      2

```

```

*hydro      delta z      vol
3430701      9.1628      1
3430702      0.      3
*
*hydro      roughness      hyd diam      vol
3430801      0.0015      0.      3
*
*hydro      f loss      r loss      jun
3430901      .257      .257      1
3430902      .468      .468      2
*
*hydro      fe      vol
3431001      0      3
*
*hydro      fvcahs      jun
3431101      000000      2
*
*hydro      ic      pressure      eq temp      vol
3431201      0      2258.0000      693.04000      1051.9000      0.00000000      0.0      01
3431202      0      2258.0000      628.19000      1051.7500      0.00000000      0.0      02
3431203      0      2258.0000      617.04000      1051.7060      0.00000000      0.0      03

```

```

*hydro      vel/flw
3431300      0
*
*hydro      f flowrate      g flowrate      j flowrate      jun
3431301      04679690      04679690      0.0      01
3431302      04636770      04636770      0.0      02
*
*      unc dia      beta      c      m
3431401      0.875      0.      1.      1.      2

```

```

*hydro      component name      component type
3440000      'porx'      valve
*-----*
*hydro      from      to      area      f loss      r loss      fvcahs
3440101      340000000      345000000      .02126      0.      0.      00100
*
*      unc dia      beta      c      m
3440110      0.0      0.      1.      1.

```

```

*hydro      vel/flw      f flowrate      g flowrate      j flowrate
3440201      0      .00000000      .00000000      0.0
*
*hydro      valve type
3440300      3rvlv
*
*hydro      contrivar      table no.
3440301      228      0

```

```

*hydro      component name      component type
3450000      'por-inl'      twdpsvl
*-----*
*hydro      area      length      volume
3450101      1.866      0.0      1.0e+06
*
*hydro      horz angle      vert angle      delta z
3450102      0.0      0.0      0.0
*
*hydro      roughness      hyd diam      fe
3450103      0.0      0.0      10
*
*hydro      ic      trip no.      alpha v70      numpic v70

```



```

3460200 01
*hydro time pressure quality
3460201 0 1.
*-----*
*hydro component name component type
3460300 "cvs-safe" valve
*-----*
*hydro from to area r loss r loss fvcatg
3460101 346005000 347000000 .04050 0. 0. 00100
*
3460110 unc dia beta c m
0.0 0. 1. 1.
*
*hydro vol/lin f flowrate g flowrate j flowrate
3460201 0 00000000 00000000 0.0
*
*hydro valve type
3460300 tripval
*
*hydro trip no.
3460301 814
*-----*
*hydro component name component type
3470000 "safetysl" tripval
*-----*
*hydro area length volume
3470101 1.0eb 0.0 1.0e+06
*
*hydro horiz angle vert angle delta z
3470102 0.0 0.0 0.0
*
*hydro roughness hyd diam fe
3470102 0.0 0.0 10
*
*hydro ic trip no. alpha vrc numeric vrc
3470200 02
*
*hydro time pressure quality
3470201 0 36. 1.
*-----*
*loop 5 clean generator secondary
*-----*
*hydro component name component type
3540000 "top of g" annulus
*-----*
*hydro no. volumes
3540001 1
*
*hydro vol area vol
3540101 0.0 1
*
*hydro length vol
3540301 7.48 1
*
*hydro volume vol
3540401 548.17 1
*
*hydro vert angle vol
3540601 -90. 1
*
*hydro roughness hyd diam vol
3540801 0.00015 0.0 1

```

```

*
*hydro fe vol
3541001 00 1
*
3541201 0 804.18000 507.43000 1115.0000 .33753000 0.0 01
*-----*
*hydro component name component type
3560000 "to feed" angljun
*-----*
*hydro from to area r loss r loss fvcatg
3560101 356010000 356000000 0.0 0.0 0.0 030000
*
3560110 unc dia beta c m
2.50 0. 1. 1.
*
3560201 0 2.0229000 1.0173000 0.0
*-----*
*hydro component name component type
3580000 "reubate" annulus
*-----*
*hydro no. volumes
3580001 1
*
*hydro vol area vol
3580101 0.0 1
*
*hydro length vol
3580201 4.400 1
*
*hydro volume vol
3580401 188.5 1
*
*hydro vert angle vol
3580601 -90. 1
*
*hydro roughness hyd diam vol
3580801 0.00010 2.75 1
*
*hydro fe vol
3581001 00 1
*
3581201 0 403.70000 400.36000 1115.0000 .06851430 0.0 01
*-----*
*hydro component name component type
3600000 "feed jun" angljun
*-----*
*hydro from to area r loss r loss fvcatg
3600101 360010000 362000000 0. 2.0 0.0 030000
*
3600110 unc dia beta c m
1.24 0. 1. 1.
*
3600201 0 5.2663000 5.1492000 0.0
*-----*
*hydro component name component type
3620000 "downcase" annulus
*-----*
*hydro no. volumes
3620001 4
*
*hydro vol area vol
3620101 17.54 1
3620110 5.266 4

```

```

*hydro length vol
3620301 7.834 4
3620302 6.016 4
*hydro volume vol
3620401 0. 4
*hydro vert angle vol
3620601 90. 4
*hydro roughness hyd diam vol
3620801 0.00015 1.24 1
3620802 0.00015 0.362 4
*hydro fe vol
3621001 00 4
*hydro vcats jun
3621101 01100 1
3621102 01000 3
3621201 0 807.23000 492.19000 1114.9000 03302890 0.0 01
3621202 0 807.91000 492.47000 1114.9000 02581430 0.0 02
3621203 0 809.96000 492.71000 1114.9000 01984860 0.0 03
3621204 0 811.80000 492.86000 1114.9000 01408570 0.0 04
3621300 0

```

```

3621301 17.362000 16.204000 0.0 01
3621302 17.227000 16.370000 0.0 02
3621303 17.130000 16.307000 0.0 03
*hydro junc dia beta c m
3621401 0.362 0. 1. 1. 3

```

```

*****
*hydro component name component type
3640000 'dr to br' sngljun
*****
*hydro from to area f loss r loss fvcats
3640101 367010000 368000000 0.0 2.4 2.4 030100
*hydro junc dia beta c m
3640110 0.126 0. 1. 1.
3640201 0 17.034000 19.627000 0.0

```

```

*****
*hydro component name component type
3660000 'sg boiler' pipe
*****
*hydro no. volumes
3660001 4
*hydro vol area vol
3660101 0.0 4
*hydro length vol
3660301 6.016 1
3660302 7.834 4
*hydro volume vol
3660401 291.2 1
3660402 367.0 2
3660403 369.4 3
3660404 383.8 4

```

```

*hydro vert angle vol
3680601 90. 4
*hydro roughness hyd diam vol
3680801 0.00015 0.126 4
*hydro f loss r loss jun
3680901 7.0 12.0 1
3680902 9.0 9.0 3
*hydro fe vol
3681001 100. 4
*hydro fvcats jun
3681101 00000 2
3681201 0 810.80000 507.91000 1114.9000 07979000 0.0 01
3681202 0 808.35000 506.18000 1114.9000 03015000 0.0 02
3681203 0 805.68000 507.90000 1115.1800 02653000 0.0 03
3681204 0 805.03000 507.62000 1115.2800 05388600 0.0 04
3681300 0
3681301 3.1943000 5.2406000 0.0 01
3681302 5.1200000 8.5943000 0.0 02
3681303 8.5185000 11.702000 0.0 03
*hydro junc dia beta c m
3681401 0.016 0. 1. 1. 3 *Hyd.Diam. of tube supp. pl.

```

```

*****
*hydro component name component type
3680000 'adv boiler' sngljun
*****
*hydro from to area f loss r loss fvcats
3680101 368010000 370000000 0.0 0.0 0.0 030000
*hydro junc dia beta c m
3680110 0.126 0. 1. 1.
3680201 0 10.703000 13.025000 0.0

```

```

*****
*hydro component name component type
3700000 'above tu' snglvol
*****
*hydro area length volume
3700101 0.0 4.405 393.5
*hydro horiz angle vert angle delta z
3700102 0.0 90. 4.405
*hydro roughness hyd diam fe
3700103 0.00015 18.53 00
3700200 0 804.53000 507.54000 1115.4800 05463000

```

```

*****
*hydro component name component type
3720000 'adv tube' sngljun
*****
*hydro from to area f loss r loss fvcats
3720101 370010000 374000000 0.0 0.0 0.0 030000
*hydro junc dia beta c m
3720110 5.190 0. 1. 1.
3720201 0 8.3903000 10.051000 0.0

```

```

*hydro component name component type
3740000 'below se' shglvol
-----*
*hydro area length volume
3740101 0.0 7.88 500.44
*
*hydro horz angle vert angle delta z
3740102 0. 90. 7.88
*
*hydro roughness hyd diam fe
3740103 0.00015 0.19 00
*
3740200 0 804.15000 507.47000 1115.2000 87890000

```

```

*hydro component name component type
3780000 'separate' separate
-----*
*hydro no. juns vel/flw
3780001 3 0
*
*hydro area length volume
3780101 0.0 5.29 697.2
*
*hydro horz angle vert angle delta z
3780102 0.0 90.0 5.29
*
*hydro roughness hyd diam fe
3780103 0.00015 0.17 00
*
3780200 0 803.28000 507.33000 1115.0000 17715000

```

```

*hydro from to area f loss r loss vcahs
3781101 378010000 382000000 0.0 127.5 127.5 01000 0.02
3782101 378000000 354000000 0.0 90.0 90.0 01000 1.0
3783101 374010000 378000000 0.0 0.0 0.0 01020
*
*hydro junc dia beta c w
3781110 1.0 0. 1. 1.
3782110 2.59 0. 1. 1.
3783110 1.0 0. 1. 1.
*
3781201 4.7352000 4.8459000 0.0
3782201 1.9379000 1.1705000 0.0
3781201 9.7989000 9.7989000 0.0

```

```

*hydro component name component type
3820000 'steam co' branch
-----*
*hydro no. juns vel/flw
3820001 1 0
*
*hydro area length volume
3820101 0.0 6.33 695.0
*
*hydro horz angle vert angle delta z
3820102 0.0 90. 6.33
*
*hydro roughness hyd diam fe
3820103 0.00015 0.167 00
*
3820200 0 801.93000 507.10000 1114.9000 1.0000000

```

```

*hydro from to area f loss r loss vcahs
3821101 382010000 850000000 1.59 1.5 1.5 00000
*
*hydro junc dia beta c w
3821110 0.187 0. 1. 1.
*
3821201 371.22000 383.28000 0.0

```

```

$loop c - includes the hot leg, steam generator inlet plenum, u-tubes,
$steam generator outlet plenum, pump suction leg, rc over, and cold leg
$loop c hot leg

```

```

*hydro component name component type
4040000 'hotleg3' pipe
-----*
*hydro no. volumes
4040001 3
*
*hydro vol area vol
4040101 0. 3
*
*hydro length vol
4040301 5.3105 3
*
*hydro volume vol
4040401 24.4874 1
4040402 24.3590 3
*
*hydro vert angle vol
4040501 0. 3
*
*hydro roughness hyd diam vol
4040801 0.00015 0. 3
*
*hydro fe vol
4041001 0 3
*
*hydro fvcchs jun
4041101 000000 2

```

```

*hydro ic pressure eq. temp vol
4041201 0 2248.2000 810.43000 1052.3000 00000000 0.0 01
4041202 0 2248.9000 810.50000 1052.3000 00000000 0.0 02
4041203 0 2248.6000 810.50000 1052.4000 00000000 0.0 03
*
*hydro vol/flw
4041300 0
*
*hydro f flowrate g flowrate j flowrate jun
4041301 47.689000 47.689000 0.0 01
4041302 47.689000 47.689000 0.0 02
*
*hydro junc dia beta c w
4041401 2.417 0. 1. 1. 2

```

```

*hydro component name component type
4050000 'hotleg4' branch
-----*
*hydro no. juns vel/flw
4050001 2 0
*
*hydro area length volume
4050101 0. 8.7932 32.1338

```

```

*hydro
4050104      hertz angle      vert angle      delta z
      0.0              26.24              3.0000
*
*hydro
4050105      roughness      hyd diam      fe
      0.015              0.0              0.0
*
*hydro
4050106      ic      stress/ft      sq      loss
      0.0              2242.3000  610.5000  1055.4000  0.0000000
*
*hydro
4051101      from      to      area      f loss      r loss      vrate
4051101      404010000      405000000      4.0      0.0      0.0      0.0000
4052101      343010000      405000000      7.0      0.0      0.0      0.0100
*
*hydro
4051110      junc dia      beta      c      e      f
4051110      2.413      0.0      1.0      1.0      1.0
4052110      0.075      0.0      1.0      1.0      1.0
*

```

```

*hydro
4051201      f flourate      y flourate      j flourate
4051201      7.889700  47.089000  0.0
4052201      0.882210  0.882210  0.0
*
$loop c steam generator inlet plenum
*

```

```

*hydro
4060000      component name      component type
      "sg inlet"      branch
*

```

```

*hydro
4060001      no. junc      vel/ftw
      2      0
*

```

```

*hydro
4070101      area      length      volume
      0.0      3.28      116.1
*

```

```

*hydro
4080102      hertz angle      vert angle      delta z
      0.0      90.0      3.28
*

```

```

*hydro
4080103      roughness      hyd diam      fe
      0.015      0.0      0.0
*

```

```

4080200      0      2790.2000  610.5000  1052.2000  0.0000000
*
*hydro
4081101      from      to      area      f loss      r loss      vrate
4081101      408010000      408000000      5.0      0.0      0.0      0.0100
4082101      408010000      408000000      10.52      0.0      0.0      0.0100
*
*hydro
4081110      junc dia      beta      c      e      f
4081110      1.052      0.0      1.0      1.0      1.0
4082110      1.05458      0.0      1.0      1.0      1.0
*

```

```

4081201      44.0  4000  -4.854100  0.0
4082201      21.710000  0.770000  0.0
*

```

```

$loop i u tubes
*

```

```

*hydro
4090000      comp. no. i name      component type
      "sg tubes"      pipe
*

```

```

*hydro
4090101      no. volines
      0
*

```

```

*hydro
4090101      vol i sq      vol
      10.11      0
*

```

```

*hydro
4090201      length      vol
      8.0      0
*

```

```

*hydro
4090401      no. vol      vol
      0.0      0
*

```

```

*hydro
4090501      vert angle      vol
      90.0      0
4090502      -90.0      0
*

```

```

*hydro
4090503      roughness      hyd diam      vol
      0.0001      0.0458      0
*

```

```

*hydro
4091001      fe      vol
      0.0      0
*

```

```

*hydro
4091101      f loss      jun
      26.100      7
*

```

```

4091101      0      2242.3000  595.0000  7111.8000  300000000  0.0      01
4091102      0      2242.3000  595.0000  7111.8000  300000000  0.0      02
4091202      0      16.607  580.18000  100.19000  300000000  0.0      03
4091204      0      20.1807  559.70000  71.05000  300000000  0.0      04
4091206      0      2.73102  551.83000  26.43000  300000000  0.0      05
4091208      0      7.02950  544.38000  105.1100  300000000  0.0      06
4091207      0      1.00000  538.04000  1055.3000  300000000  0.0      07
4091209      0      2204.1100  522.53000  1055.5000  300000000  0.0      08
4091300      0
*

```

```

4091301      20.3100  0.20  2.100  0.0      01
4091302      12.6100  0.10  1.000  0.0      02
4091303      10.8100  0.05  0.500  0.0      03
4091304      10.1300  0.04  0.400  0.0      04
4091305      10.2400  0.04  0.400  0.0      05
4091306      10.0800  0.04  0.400  0.0      06
4091307      10.9500  0.05  0.500  0.0      07
*

```

```

*hydro
4100000      comp. name      component type
      "sg inlet"      branch
*

```

```

*hydro
4100001      no. junc      vel/ftw
      2      0
*

```

```

*hydro
4100101      area      length      volume
      0.0      3.28      116.1
*

```

```

*hydro
4100102      hertz angle      vert angle      delta z
      0.0      -90.0      3.28
*

```

```

*hydro
4100103      roughness      hyd diam      fe
      0.0001      0.0      0.0
*

```

```

4100200      0      2204.3000  593.54000  1055.5000  0.0000000
*

```

```

*hydro
4101101      from      to      area      f loss      r loss      vrate
4101101      410010000      410000000      4.0      0.0      0.0      0.0100
4102101      408010000      410000000      10.52      0.0      0.0      0.0100
*

```

```

*hydro
4101110      junc dia      beta      c      e      f
4101110      2.432      0.0      1.0      1.0      1.0
4102110      0.05458      0.0      1.0      1.0      1.0
*

```

```

4101201 35.841000 35.841000 0.0
4102201 18.856000 18.856000 0.0
*.....*
loop c pump suction leg
*
*hydro component name component type
410000 'rcsuctio' pipe
*
*hydro no. volumes
412001 5
*
*hydro vol area vol
4120101 5
*
*hydro length vol
4120201 4.8599 1
4120302 2.7219 2
4120303 7.1209 3
4120304 4.2250 4
4120305 7.1209 5
*
*hydro volume vol
4120401 27.4002 1
4120402 14.2667 2
4120403 27.3240 3
4120404 22.1451 4
4120405 27.3240 5
*
*hydro vert angle vol
4120501 90 1
4120502 -90 2
4120503 -30.54 3
4120504 0 4
4120505 30.54 5
*
*hydro delta z vol
4120701 -4.2952 1
4120702 -1.7219 2
4120703 -4.5233 3
4120704 0 4
4120705 4.5233 5
*
*hydro roughness hyd diam vol
4120801 .0015 1. 5
*
*hydro f loss r loss jun
4120901 .053 .053 1
4120902 0 0 2
4120903 .1 .1 4
*
*hydro te vol
4121001 0 5
*
*hydro fvcatn jun
4121101 000000 4
*
*hydro ic pressure eq. temp vol
4121201 0 2194.8000 533.54000 1056.2000 60000000 0.0 01
4121202 0 2194.9000 533.54000 1056.2000 00000000 0.0 02
4121203 0 2196.0000 533.54000 1056.1000 00000000 0.0 03
4121204 0 2195.8000 533.54000 1056.1000 00000000 0.0 04
4121205 0 2194.2000 533.55000 1056.2000 00000000 0.0 05
*

```

```

*hydro vel/flw
4121300 0
*
*hydro f flowrate g flowrate j flowrate jun
4121301 37.884000 37.884000 0.0 01
4121302 37.884000 37.884000 0.0 02
4121303 37.884000 37.884000 0.0 03
4121304 37.884000 37.884000 0.0 04
*
*hydro junc dia beta c m A
4121401 2.583 0 1 1 4
*
*.....*
loop c reactor coolant pump
*
*hydro component name component type
4140000 'c rcp' pump
*
*hydro area length volume
4140101 0.0 4.0583 163.7136
*
*hydro horz angle vert angle delta z
4140102 0 90.0 4.0583
*
*hydro equil flow
4140103 0
*
*hydro from jun area f loss r loss fvcatn
4140108 412010000 5.2414 0.0 0.0 00000
*
*hydro to jun area f loss r loss fvcatn
4140109 416000000 4.1247 0.0 0.0 00000
*
*hydro junc dia beta c m A
4140110 2.583 0 1 1 1
4140111 2.282 0 1 1 1
*
*hydro ic pressure eq. temp
4140200 0 2250.5000 533.62000 1062.2000 60000000
*
*hydro vel/flw f flowrate g flowrate j flowrate
4140201 0 37.885000 37.885000 0.0
4140202 0 48.123000 48.123000 0.0
*
*hydro ptol zfaci diff i tort j pvel k tripp no. rvs i
4140301 214 214 2 2 214 221 221 0
4140302 1140.0000 1.9432779 88500.000 277.88000 23.000 000 70000 880
4140303 47.180000 60000000 60000000 235.00000 25.900000 00000000
*
*hydro rated pump vel. unit/rated vel. rated flow rated head
*
*hydro rated torque mom of inertia rated dens air torque
*
*hydro coeff. f12 coeff. f10 coeff. f11 coeff. f13
*
*.....*
loop c pump discharge and cold leg
*
*hydro component name component type
4160000 'pumpd.53' anglvol
*
*hydro area length volume
4160101 4.1247 8.9233 0.
*
*hydro horz angle vert angle delta z
4160102 0 0 0.
*

```



```

*hydro roughness hyd diam fe
4180103 .00015 0. 00
*
*hydro ic pressure eq temp
4180200 0 2299.0000 533.62000 1049.6000 00000000
*
*hydro component name component type
4180000 'sumpdia3' branch
*
*hydro no. junk vel/flw
4180001 4 0
*
*hydro area length volume
4180101 4.1247 5.4584 0.
*
*hydro horz angle vert angle delta z
4180102 0. 0. 0.
*
*hydro roughness hyd diam fe
4180103 .00015 0. 00
*
*hydro ic pressure eq temp
4180200 0 2299.1000 533.62000 1049.6000 00000000
*
*hydro from to area f loss r loss vcatb
4181101 418010000 418000000 4.1247 0. 0. 00000
4182101 418010000 420000000 4.1247 0. 0. 00000
4183101 823010000 418000000 3941 0. 0. 00100
4184101 418000000 337000000 0645 0. 0. 00100
*
*hydro junc dia beta c w
4181110 2.292 0. 1. 1.
4182110 2.292 0. 1. 1.
4183110 0.0 0. 1. 1.
*
*hydro f flowrate g flowrate j flowrate
4181201 48.107000 48.107000 0.0
4182201 48.109000 48.101700 0.0
4183201 01125390 01125390 0.0
4184201 178166.3 178166.3 0.0
*
*hydro component name component type
4200000 'sumpdia3' pipe
*
*hydro no. volumes
4200001 2
*
*hydro vol area vol
4200101 0. 2
*
*hydro junc area junc
4200201 4.1247 1
*
*hydro length vol
4200301 5.4584 1
4200302 5.4584 2
*
*hydro volume vol
4200401 22.5143 1
4200402 26.4377 2
*
*hydro vert angle vol
4200501 0. 2
*

```

```

*hydro roughness hyd diam vol
4200801 .00015 0.0 2
*
*hydro f loss r loss junc
4200901 .029 .029 1
*
*hydro fe vol
4201001 0 2
*
*hydro fvcatb junc
4201101 000000 1
*
*hydro ic pressure eq temp vol
4201201 0 2299.4000 533.62000 1049.6000 00003000 0.0 01
4201202 0 2291.8000 533.62000 1047.3000 00000000 0.0 02
*
*hydro vel/flw
4201300 0
*
*hydro f flowrate g flowrate j flowrate junc
4201301 48.109000 48.109000 0.0 01
*
*hydro junc dia beta c w
4201401 2.292 0. 1. 1. 1
*
*loop c steam generator secondary
*
*hydro component name component type
4540000 'top of d' annulus
*
*hydro no. volumes
4540001 1
*
*hydro vol area vol
4540101 0.0 1
*
*hydro length vol
4540201 7.88 1
*
*hydro volume vol
4540301 548.17 1
*
*hydro vert angle vol
4540401 .00 1
*
*hydro roughness hyd diam vol
4540501 0.00015 0.0 1
*
*hydro fe vol
4541001 00 1
*
4541201 0 805.90000 507.73000 1115.9000 3*069000 0.0 01
*
*hydro component name component type
4560000 'to feed' shgion
*
*hydro from to area f loss r loss fvcatb
4560101 4541000 458000000 0.0 0.0 0.0 0.0 030000
*
*hydro junc dia beta c w
4560110 2.50 0. 1. 1.
*
4560201 0 3.8223000 1.024000 0.0
*

```

```

*hydro
4580000 component name component type
         'feetale' stimulus
-----*
*hydro
4580001 no. volumes
         1
*
*hydro
4580101 vol area
         0.0
         vol
*
*hydro
4580301 length
         4.405
         vol
*
*hydro
4580401 volume
         180.5
         vol
*
*hydro
4580601 vert angle
         90.
         vol
*
*hydro
4580801 roughness hyd dia
         0.00015 1.54
         vol
*
*hydro
4581001 fe
         00
         vol
*
4581201 0 807.44000 491.59000 1114.9000 06703800 0.0 01
*

```

```

*****
*hydro
4600000 component name component type
         'feet jun' stimulus
-----*
*hydro
4600101 from to area f loss r loss fvcats
         462010000 462000000 0. 7.0 3.0 03000
         unc dia beta c e
         1.24 0. 1. 1.
*
4600201 0 5.667900 1487.0 0.0

```

```

*****
*hydro
4620000 component name component type
         'downcase' stimulus
-----*
*hydro
4620001 no. volumes
         4
*
*hydro
4620101 vol area
         17.94
         vol
*
*hydro
4620102 5.569
         vol
*
*hydro
4620301 length
         7.834
         vol
*
*hydro
4620302 8.016
         vol
*
*hydro
4620401 volume
         0.
         vol
*
*hydro
4620601 vert angle
         90.
         vol
*
*hydro
4620801 roughness hyd dia
         0.00015 1.24
         vol
*
*hydro
4620802 0.00015 0.362
         vol
*
*hydro
         fe
         vol

```

```

4621001 00
         4
*
*hydro
4621101 vcats
         0100
         jun
*
4621102 01000
         3
*
4621201 0 808.95000 492.49000 1114.9000 02650000 0.0 01
4621202 0 809.63000 492.78000 1114.9000 02627500 0.0 02
4621203 0 811.68000 493.02000 1114.9000 02021130 0.0 03
4621204 0 813.52000 493.17000 1114.9000 01434500 0.0 04
4621300 0
*
4621301 17.251000 16.190000 0.0 01
4621302 17.214000 16.363000 0.0 02
4621303 17.118000 16.289000 0.0 03
*
4621401 0.362 0. 1. 1. 3

```

```

*****
*hydro
4640000 component name component type
         'dc to bo' stimulus
-----*
*hydro
4640101 from to area f loss r loss fvcats
         462010000 462000000 0.0 2.4 2.4 030100
         unc dia beta c e
         0.128 0. 1. 1.
*
4640201 0 17.017000 19.074000 0.0

```

```

*****
*hydro
4660000 component name component type
         'up boiler' pipe
-----*
*hydro
4660001 no. volumes
         4
*
*hydro
4660101 vol area
         0.0
         vol
*
*hydro
4660301 length
         6.010
         vol
*
*hydro
4660302 7.804
         vol
*
*hydro
4660401 volume
         291.2
         vol
*
4660402 367.0
         vol
*
4660403 369.4
         vol
*
4660404 383.8
         vol
*
*hydro
4660601 vert angle
         90.
         vol
*
*hydro
4660801 roughness hyd dia
         0.00015 0.125
         vol
*
*hydro
4660901 f loss r loss
         12.0 12.0
         jun
*
4660902 0.0 0.0
         3
*
*hydro
4661001 fe
         100
         vol
*
*hydro
4661101 fvcats
         000000
         jun
*
4661201 0 811.80000 508.29000 1114.9000 37805000 0.0 01

```

```

4661202 0 810.07000 508.48000 1114.8000 43539000 0.0 03
4661203 0 808.40000 508.10000 1115.1000 43596000 0.0 03
4661204 0 806.76000 507.82000 1115.2000 43573000 0.0 04
*
4661306 0
*
4661301 3.1866000 5.2367000 0.0 01
4661302 5.1042000 5.5622000 0.0 02
4661303 6.5570000 11.657000 0.0 03
*
*hydro compoent name component type
4660000 "abv tube" angljun
*
*hydro from to area r loss r loss vrate
4660101 466010000 470000000 0.0 0.0 0.0 030000
*
*hydro junc dia beta c m
4660110 0.120 0. 1. 1.
*
4680201 0 10.658000 12.971000 0.0
*
*hydro component name component type
4700000 "above su" anglval
*
*hydro area length volume
4700101 0.0 4.405 382.5
*
*hydro horz angle vert angle delta z
4700102 0.0 90. 4.405
*
*hydro roughness hyd diam fe
4700103 0.00015 10.53 00
*
4700200 0 806.26000 507.83000 1115.4000 40410000
*
*hydro component name component type
4720000 "abv tube" angljun
*
*hydro from to area r loss r loss vrate
4720101 470010000 474900000 0.0 0.0 0.0 030000
*
*hydro junc dia beta c m
4720110 0.190 0. 1. 1.
*
4720201 0 8.2647000 10.009000 0.0
*
*hydro component name component type
4740000 "below su" anglval
*
*hydro area length volume
4740101 0.0 7.59 500.54
*
*hydro horz angle vert angle delta z
4740102 0. 90. 7.59
*
*hydro roughness hyd diam fe
4740103 0.00015 5.19 00
*
4740200 0 805.98000 507.77000 1115.1000 27649000
*
*hydro component name component type
4760000 "spvrtlg" angljun

```

```

*hydro no. junc vel/fw
4780001 3 0
*
*hydro area length volume
4780101 0.0 1.29 697.2
*
*hydro horz angle vert angle delta z
4780102 0.0 90.0 1.29
*
*hydro roughness hyd diam fe
4780103 0.00015 0.17 00
*
4780200 0 805.01000 507.62000 1115.0000 17956000
*
*hydro from to area r loss r loss vrate
4781101 478010000 482000000 0.0 127.5 127.5 01000 0.02
4782101 478000000 454000000 0.0 90.0 90.0 01000 1.0
4783101 474010000 478000000 0.0 0.0 0.0 01020
*
*hydro junc dia beta c m
4781110 1.0 0. 1. 1.
4782110 2.59 0. 1. 1.
4783110 1.0 0. 1. 1.
*
4791201 4.7100000 4.9214000 0.0
4792201 1.3401000 1.1726000 0.0
4793201 9.7575000 9.1275000 0.0
*
*hydro component name component type
4820000 "steak do" brnch
*
*hydro no. junc vel/fw
4820001 1 0
*
*hydro area length volume
4820101 0.0 0.53 699.0
*
*hydro horz angle vert angle delta z
4820102 0.0 90. 0.53
*
*hydro roughness hyd diam fe
4820103 0.00015 0.167 00
*
4820200 0 803.67000 507.39000 1114.9000 10000000
*
*hydro from to area r loss r loss vrate
4821101 482010000 750000000 1.20 1.5 1.0 1000
*
*hydro junc dia beta c m
4821110 0.167 0. 1. 1.
*
4821201 367.17000 361.29000 0.0
*
$
$ Main feedwater lines for steam generator a,b, and c from the feedwater
$ header to each steam generator. Includes motor and steam driven
$ auxiliary feedwater system.
$
$
$
$ Line a feedwater regulating valve
$
*hydro component name component type

```

```

5050000      'reg xlv 1      valve
*-----*
*hydro from to area f loss r loss vcats
5050101 520010000 510000000 1.0596 0.0 0.0 00000
*
* hydro val/flw f flowrate g flowrate j flowrate
5050201 0 16.939000 16.939000 0.0
*
*hydro valve type
5050300
*
*hydro ctrl/val table no.
5050301 520 0
*
*hydro area/posn f csurv r csurv
5050401 0.0 0.0 0.0
5050402 0.75 589.3943 0.0
5050403 1.0 960.3239 0.0
*-----*
$line a steam turbine auxfeed connection volume
*-----*
*hydro component name component type
5100000 'aux in' singlvol
*-----*
*hydro area length volume
5100101 1.0596 0.0 193.3770
*
*hydro horz angle vert angle delta z
5100102 0.0 0.0 0.0
*
*hydro roughness hyd diam fe
5100103 0.00015 1.1615 00
*
*hydro ic pressure energy quality
5100200 0 846.79000 417.50700 1114.1000 00000000
*-----*
*hydro component name component type
5150000 'chk xlv 1' valve
*-----*
*hydro from to area f loss r loss vcats
5150101 510010000 520000000 1.0596 7.5365 7.5365 00000
*
*hydro val/flw f flowrate g flowrate j flowrate
5150201 0 16.956000 16.956000 0.0
*
*hydro valve type
5150300
*
*hydro chkxlv type init posn back press leak ratio
5150301 0 0 0 0
*-----*
$line a piping from motor driven auxfeed connection to steam
$generator a
*-----*
*hydro component name component type
5200000 'aux in' singlvol
*-----*
*hydro area length volume
5200101 1.0596 0.0 204.6139
*
*hydro horz angle vert angle delta z

```

```

5200102 0.0 0.0 0.0
*
*hydro roughness hyd diam fe
5200103 0.00015 1.1615 00
*
*hydro ic pressure energy quality
5200200 0 831.30000 417.51000 1114.5000 00000000
*-----*
$junction connecting feed line a to steam generator a
$model as a trip valve
*-----*
*hydro component name component type
5250000 'jun fw a' valve
*-----*
*hydro from to area f loss r loss vcats
5250101 520010000 510000000 0.175 11.3909 11.3909 00100
*
* hydro val/flw f flowrate g flowrate j flowrate
5250201 0 16.957000 17.031000 0.0
*
*hydro valve type
5250300
*
*hydro trip no.
5250301 707
*-----*
$steam generator a motor and steam driven auxfeed lines
$model as check valves with line resistance
*-----*
*hydro component name component type
5300000 'a aux a' valve
*-----*
*hydro from to area f loss r loss vcats
5300101 532010000 510000000 0.0799 6.296 6.296 00000
*
* hydro val/flw f velocity g velocity j velocity
5300201 0 00007000 00000000 0.0
*
*hydro valve type
5300300
*
*hydro chkxlv type init posn back press leak ratio
5300301 0 0 0 0
*-----*
$main header for the steam driven auxfeed system
*-----*
*hydro component name component type
5350000 'b aux hd' singlvol
*-----*
* hydro val/flw f flowrate g flowrate j flowrate
5350101 0 0.0 0.0 0.0
*
*hydro area length volume
5350101 0.1810 0.0 12.1865
*
*hydro horz angle vert angle delta z
5350102 0.0 0.0 0.0

```







```

5800201 0 .00000000 .0000000 0.0
*
*hydro valve type
5800300 srvlv
*
*hydro ctrlvr table no.
5800301 0
*
*****
*hydro component name component type
5800000 'cond 1' 'sdprvl'
*
*hydro area length volume
5800101 1.0e+06 0.0 1.0e+06
*
*hydro horz angle vert angle delta z
5800102 0.0 0.0 0.0
*
*hydro roughness hyd diam fe
5800103 0.0 0.0 10
*
*hydro ic trip no. alpha vrc numeric vrc
5800200 02
*
*hydro time pressure quality
5800201 0.0 14.7 1.0
*****
main feedwater line b from header to steam generator b
*
*hydro component name component type
6050000 'reg vlv' valve
*
*hydro from to area f loss r loss vcase
6050101 878010000 878000000 1.0596 0.0 0.0 00000
*
*hydro junc dia beta c w
6050110 0.0 0. 1. 1.
*
*hydro vel/flw f flowrate g flowrate j flowrate
6050201 0 16.990070 16.990000 0.0
*
*hydro valve type
6050300 srvlv
*
*hydro ctrlvr tabl no.
6050301 0
*
*hydro area/posn f csbvt r csbvt
6050401 0.0 0.0 0.0
6050402 0.75 589.7943 0.0
6050403 1.0 967.3239 0.0
*****
*hydro component name component type
6100000 'aux in' shglvcl
*
*hydro area length volume
6100101 1.0596 0.0 188.1088
*
*hydro horz angle vert angle delta z
6100102 0.0 0.0 0.0
*
*hydro roughness hyd diam fe
6100103 0.00015 1.1615 00

```

```

*
*hydro ic pressure energy quality
6150200 0 842.88000 417.50000 1114.2000 .00000000
*****
*hydro component name component type
6150000 'chkvly b' valve
*
*hydro from to area f loss r loss vcase
6150101 610010000 620000000 1.0596 3.5365 7.5365 00000
*
*hydro junc dia beta c w
6150110 0.0 0. 1. 1.
*
*hydro vel/flw f flowrate g flowrate j flowrate
6150201 0 17.007000 17.007000 0.0
*
*hydro valve type
6150300 chkvly
*
*hydro chkvly type init posn back press leak ratio
6150301 0 0 0 0
*****
*hydro component name component type
6200000 'aux in' shglvcl
*
*hydro area length volume
6200101 1.0596 0.0 92.4309
*
*hydro horz angle vert angle delta z
6200102 0.0 0.0 0.0
*
*hydro roughness hyd diam fe
6200103 0.00015 1.1615 00
*
*hydro ic pressure energy quality
6200200 0 829.27000 417.51000 1114.5000 .00000000
*****
junction connecting s/w line b to steam generator b
*model as a trip valve
*
*hydro component name component type
6250000 'jun tw b' valve
*
*hydro from to area f loss r loss vcase
6250101 620010000 650000000 0.7175 11.2908 11.9909 00100
*
*hydro junc dia beta c w
6250110 0.0 0. 1. 1.
*
*hydro vel/flw f flowrate g flowrate j flowrate
6250201 0 17.009000 17.040000 0.0
*
*hydro valve type
6250300 tripvlv
*
*hydro trip no.
6250301 109
*****
steam driven auxfeed water line for sgb
*
*hydro component name component type
6300000 's aux b' valve
*
*hydro from to area f loss r loss vcase
6300101 632010000 670000000 0.0799 5.593 5.593 00000
*
*hydro junc dia beta c w

```

```

6300110 0.0 0. 0. 1. 1.
*hydro vel/flw f velocity g velocity j velocity
6300201 0 .00100754 .00100254 0.0
*hydro valve type
6300300 chkvly
*hydro chkvly type init push back press leak ratio
6300301 0 0 0 0 0
$main steam line b - from steam generator b to steam header - /includes $
$sixv safety valves and purv's associated with steam line b $
*hydro component name component type
6400000 'six v' valve
*hydro from to area f loss g loss vchgs
6400101 542010000 520000000 0.0790 15.44 15.44 00000
* hydro junction dia beta c s
6400110 0.0 0. 1. 1.
*hydro vel/flw f flowrate g flowrate j flowrate
6400201 0 .0000000 .0000000 0.0
*hydro valve type
6400300 chkvly
*hydro chkvly type init push back press leak ratio
6400301 0 0 0 0 0
$main steam line b - from steam generator b to steam header - /includes $
$sixv safety valves and purv's associated with steam line b $
*hydro component name component type
6500000 'six b1' ang'val
*hydro area length volume
6500101 3.0940 199.1628 0.0
*hydro horiz angle vert angle delta z
6500102 0.0 0.0 0.0
*hydro roughness hyd diam fe
6500103 0.00015 1.9848 00
*hydro ic pressure energy quality
6500200 0 757.21000 490.20000 1115.0000 099900000
$main steam isolation valve b $
*hydro component name component type
6500000 'six v b' valve
*hydro from to area f loss g loss vchgs
6500101 650010000 600000000 3.0940 0.08 0.08 00100
* hydro junction dia beta c s
6500110 0.0 0. 1. 1.
*hydro vel/flw f flowrate g flowrate j flowrate
6500201 0 164.15000 161.63000 0.0
*hydro valve type
6500300 sixvly

```

```

*hydro open trip close trip change rate init push table no.
6600301 883 862 0.2857 1 0
$main steam line b from sixv to header tank $
*hydro component name component type
6600000 'six b2' ang'val
*hydro area length volume
6600101 3.0940 20.0 0.0
*hydro horiz angle vert angle delta z
6600102 0.0 0.0 0.0
*hydro roughness hyd diam fe
6600103 0.00015 1.9848 00
*hydro ic pressure energy quality
6600200 0 750.27000 490.09000 1115.0000 099900000
$check valve $
*hydro component name component type
6600000 'six v b1' valve
*hydro from to area f loss g loss vchgs
6600101 660010000 600000000 3.0940 1.8170 1.8170 00100
* hydro junction dia beta c s
6600110 0.0 0. 1. 1.
*hydro vel/flw f flowrate g flowrate j flowrate
6600201 0 106.74000 103.19000 0.0
*hydro valve type
6600300 chkvly
*hydro chkvly type init push back press leak ratio
6600301 0 0 0 0 0
$main steam line b safety valve and purv $
*hydro component name component type
6700000 'six vlv' valve
*hydro from to area f loss g loss vchgs
6700101 670010000 675000000 0.3760 0.0 0.0 00100
* hydro junction dia beta c s
6700110 0.0 0. 1. 1.
*hydro vel/flw f flowrate g flowrate j flowrate
6700201 0 .00000000 .00000000 0.0
*hydro valve type
6700300 sixvly
*hydro driver table no.
6700301 656 0
$main steam line b safety valve and purv $
*hydro component name component type
6700000 'six vlv' ang'val
*hydro area length volume
6700101 1.0e+06 0.0 1.0e+06

```

```

*
*hydro      horz angle  vert angle  delta z
$750102    0.0          0.0          0.0
*
*hydro      roughness  hyd diam   fe
$750103    0.0          0.0          10
*
*hydro ic   trip no.    alpha vrc   numeric vrc
$750200    02
*
*hydro time  pressure  quality
$750201    0.0          14.7         1.0
$*****
*hydro      component name  component type
$800000    'serv b'                valve
*
*hydro      from          to          area      f loss   r loss   vchgs
$80010    800010000    085000000    0.0578952  0.0      0.0      00100
*
*      junc dia  beta    c      m
*      0.0      0.      1.      1.
*
*hydro      vel/flw      f flowrate  g flowrate  j flowrate
$800201    0          .00000000  00000000  0.0
*
*hydro      valve type
$800300    servlv
*
*hydro      ctrlivar  table no.
$800301    029         0
*
$*****
*hydro      component name  component type
$850000    'cond b'                'ndprvl
*
*hydro      area          length      volume
$850101    1.0e+08    0.0        1.0e+08
*
*hydro      horz angle  vert angle  delta z
$850102    0.0          0.0          0.0
*
*hydro      roughness  hyd diam   fe
$850103    0.0          0.0          10
*
*hydro ic   trip no.    alpha vrc   numeric vrc
$850200    02
*
*hydro time  pressure  quality
$850201    0.0          14.7         1.0
$*****
$main feed line c from the wfw header to steam generator c
*
*hydro      component name  component type
7050000    'reg vlv'                valve
*
*hydro      from          to          area      f loss   r loss   vchgs
7050101    078010000    710000000    1.0596    0.0      0.0      00000
*
*      junc dia  beta    c      m
*      0.0      0.      1.      1.
*
*hydro      vel/flw      f flowrate  g flowrate  j flowrate
7050201    0          16.957000  16.957000  0.0
*
*hydro      valve type
7050300    servlv
*
*hydro      ctrlivar  table no.
7050301    729         0
*
*hydro      area/posn  f csurv   r csurv
7050401    0.0        0.0        0.0
7050402    0.75       1.0 0.3943  0.0
7050403    1.0        982.3239   0.0
$*****
*hydro      component name  component type
7100000    'aux ln'                'nglvcl
*
*hydro      area          length      volume
7100101    1.0596    0.0        280.9052
*
*hydro      horz angle  vert angle  delta z
7100102    0.0          0.0          0.0
*
*hydro      roughness  hyd diam   fe
7100103    0.00015   1.1815     00
*
*hydro ic   pressure  energy  quality
7100200    0          845.13000  417.51000  1114.2000  00000000
$*****
*hydro      component name  component type
7150000    'chkvly c'                valve
*
*hydro      from          to          area      f loss   r loss   vchgs
7150101    710010000    720000000    1.0596    7.5365   7.5365   00000
*
*      junc dia  beta    c      m
*      0.0      0.      1.      1.
*
*hydro      vel/flw      f flowrate  g flowrate  j flowrate
7150201    0          16.974000  16.974000  0.0
*
*hydro      valve type
7150300    chkvly
*
*hydro      chkvly type  init  posn  back press  leak ratio
7150301    0          0          0          0
$*****
*hydro      component name  component type
7200000    'aux ln'                'nglvcl
*
*hydro      area          length      volume
7200101    1.0596    0.0        87.2061
*
*hydro      horz angle  vert angle  delta z
7200102    0.0          0.0          1.0
*
*hydro      roughness  hyd diam   fe
7200103    0.00015   1.1815     00
*
*hydro ic   pressure  energy  quality
7200200    0          829.85000  417.62000  1114.5070  00000000
$*****
$junction connecting wfw line c to steam generator c
$model as a trip valve
*
*hydro      component name  component type
7250000    'jun fw c'                valve
*
*hydro      from          to          area      f loss   r loss   vchgs

```





```

*hydro component name component type
7700000 'sfly vlv' valve
-----*
*hydro from to area f loss r loss vcate
7700101 750010000 775000000 0.3700 0.0 0.0 00100
* junc dia beta c w
7700110 0.0 0. 1. 1.
*
*hydro vel/flw f flowrate g flowrate j flowrate
7700201 0 .00000000 .00000000 0.0
*
*hydro valve type
7700300 srvlv
*
*hydro ctrlr/val table no.
7700301 750 0
-----*
*hydro component name component type
7750000 'stlck c' lsdvcl
-----*
*hydro area length volume
7750101 1.0e+06 0.0 1.0e+06
*
*hydro horz angle vert angle delta z
7750102 0.0 0.0 0.0
*
*hydro roughness hyd diam fe
7750103 0.0 0.0 10
*
*hydro ic trip no. alpha vrc numeric vrc
7750200 02
*
*hydro time pressure quality
7750201 0.0 14.7 1.0
-----*
*hydro component name component type
7800000 'purv c' valve
-----*
*hydro from to area f loss r loss vcate
7800101 750010000 785000000 0.0978952 0.0 0.0 00100
* junc dia beta c w
7800110 0.0 0. 1. 1.
*
*hydro vel/flw f flowrate g flowrate j flowrate
7800201 0 .00000000 .00000000 0.0
*
*hydro valve type
7800300 srvlv
*
*hydro ctrlr/val table no.
7800301 856 0
-----*
*hydro component name component type
7850000 'cund c' lsdvcl
-----*
*hydro area length volume
7850101 1.0e+06 0.0 1.0e+06
*
*hydro horz angle vert angle delta z
7850102 0.0 0.0 0.0
*
*hydro roughness hyd diam fe
7850103 0.0 0.0 10
*
*hydro ic trip no. alpha vrc numeric vrc
7850200 02
*
*hydro time pressure quality
7850201 0.0 14.7 1.0
-----*

```

```

$line header tank
-----*
*hydro component name component type
8000000 'sta hdr' branch
-----*
*hydro no. junc vel/flw
8000001 1 0
*
*hydro area length volume
8000101 24.1196 0.0 261.7045
*
*hydro horz angle vert angle delta z
8000102 0.0 0.0 0.0
*
*hydro roughness hyd diam fe
8000103 0.00015 5.5417 00
*
*hydro ic pressure energy quality
8000200 0 781.95000 490.50000 1116.1000 99901000
*
*hydro from to area f loss r loss vcate
8000101 800010000 802000000 9.5252 0.0 0.0 00100
* junc dia beta c w
8000110 0.0 0. 1. 1.
*
*hydro f flowrate g flowrate j flowrate
8000201 186.57000 170.89000 0.0
-----*
$main steam line from turbine header to turbine stop valves
$
-----*
*hydro component name component type
8020000 'stlp' lsdvcl
-----*
*hydro area length volume
8020101 9.5252 0.0 1222.6500
*
*hydro horz angle vert angle delta z
8020102 0.0 0.0 0.0
*
*hydro roughness hyd diam fe
8020103 0.00015 2.4625 00
*
*hydro ic pressure energy quality
8020200 0 793.44000 420.00000 1116.1000 99901000
-----*
*hydro component name component type
8040000 'trbn stp' valve
-----*
*hydro from to area f loss r loss vcate
8040101 802010000 806000000 9.5252 0.0 0.0 00000
8040101 802010000 806000000 7.9220 0.0 0.0 00000
* junc dia beta c w
8040110 0.0 0. 1. 1.
*

```

```

*hydro vel/flw f flowrate g flowrate j flowrate
8040201 0 .30 13000 241 26000 0.0
*
*hydro valve type
8040300
*
*hydro ctrlvar table no.
8040301 824 0
*
*hydro area/posn f csbvy r csbvy
8040401 0.0 0 0.0
8040402 1.0 2719 4143 0.0
8040403 1.0 4963 1329 0.0
8040404 1.0 6120 2118 0.0
8040405 1.0 9594 3351 0.0
8040406 1.0 9357 2735 0.0
$*****
*hydro component name component type
8060000 'trn n' 'trdpvol'
*
*hydro area length volume
8060101 1.0e+06 0.0 1.0e+06
*
*hydro horz angle vert angle delta z
8060102 0.0 0.0 0.0
*
*hydro roughness hyd diam fe
8060103 0.0 0.0 10
*
*hydro ic trip no. alpha vrc numeric vrc
8060200 02 0 0 93
8060200 02
*
*hydro nom s pressure quality
8060201 15.0 15.0 0.9975
8060202 553.00 553.0 0.9975
8060202 0.0 553.0 0.9975
$*****
$main steam line steam dump system $
*hydro component name component type
8080000 'stm dmp' valve
*
*hydro from to area f loss r loss vcsht
8080101 802010000 810000000 0.68206 0.0 0.0 00100
*
*hydro junc dia beta c e
8080110 0.0 0. 1. 1.
*
*hydro vel/flw f flowrate g flowrate j flowrate
8080201 0 .00000000 .00000000 0.0
*
*hydro valve type
8080300
*
*hydro ctrlvar table no.
8080301 850 808
*
$*****
*hydro component name component type
8100000 'cond n' 'trdpvol'
*
*hydro area length volume
8100101 1.0e+06 0.0 1.0e+06

```

```

*hydro horz angle vert angle delta z
8100102 0.0 0.0 0.0
*
*hydro roughness hyd diam fe
8100103 0.0 0.0 10
*
*hydro ic trip no. alpha vrc numeric vrc
8100200 02
*
*hydro time pressure quality
8100201 0.0 1.5 1.0
$*****
$condensate and main feedwater piping - from the hotwell to the main $
$feedwater header, condensate piping includes the hotwell condensate $
$umps, lp heaters, heater drain pumps, lp heater bypass, and mfw pump $
$uction header, feedwater piping includes the mfw pumps, lp heaters, $
$and the main feedwater header. $
$*****
$condenser hotwell $
*hydro component name component type
8220000 'hotwell' 'trdpvol'
*
*hydro area length volume
8220101 9.333 0.0 1.0e+06
*
*hydro horz angle vert angle delta z
8220102 0.0 0.0 0.0
*
*hydro roughness hyd diam fe
8220103 0.0 0.0 10
*
*hydro ic trip no. alpha vrc numeric vrc
8220200 02
*
*hydro time pressure quality
8220201 0.0 1.5 0.0
$*****
$condensate pump - combines pump a and pump b $
*hydro component name component type
8240000 'cond pnc' pump
*
*hydro area length volume
8240101 2.4053 11.5 0.0
*
*hydro horz angle vert angle delta z
8240102 0.0 0.0 0.0
*
*hydro equil flag
8240103 0
*
*hydro from junc area f loss r loss vcsht
8240108 822000000 9.333 0.0 0.0 00000
*
*hydro to junc area f loss r loss vcsht
8240109 821000000 2.4053 0.0 0.0 00000
*
*hydro junc dia beta c e
8240110 0.0 0. 1. 1.
8240111 0.0 0. 1. 1.
*
*hydro ic pressure energy quality

```

```

8240200 0 268.54000 70.37000 1116.4000 00000000
*hydro vel/flow f flowrate g flowrate j flowrate
8240201 0 3.5042000 3.5042000 0.0
*hydro vel/flow f flowrate g flowrate j flowrate
8240202 0 13.588000 13.588000 0.0
*hydro ptdi 2fa21 diff i torq i svel i tripp no. svrs i
8240301 0 -1 -3 -1 -1 -1 625 0
8240302 1170.0000 1.0000000 19200.000 1130.0000 28280.809 2686.0000
8240303 62.400000 0.0000000 0.0000000 282.800000 28.280000 0.0000000
*hydro rated pump vel. init/rated vel. rated flow rated head
*hydro rated torque mom of inertia rated dens air torque
*hydro coeff. f12 coeff. f10 coeff. f11 coeff. f13
*hydro curve type regime
8241100 1 1
*hydro v/a head $normal (+q,*)
8241101 0.0 1.3982
8241102 0.1042 1.3928
8241103 0.2083 1.3806
8241104 0.3125 1.3607
8241105 0.4167 1.3222
8241106 0.5208 1.1858
8241107 0.6250 1.1460
8241108 0.7292 1.1150
8241109 0.8333 1.0798
8241110 0.9375 1.0354
8241111 1.0000 1.0000
*hydro curve type regime
8241200 1 2
*hydro a/v head $normal (+q,*)
8241201 0.0000 -0.3000
8241202 0.5000 0.0000
8241203 0.6250 0.1680
8241204 0.7140 0.4300
8241205 0.8000 0.5041
8241206 0.8728 0.6876
8241207 0.9600 0.9052
8241208 1.0000 1.0000
*hydro curve type regime
8241300 1 3
*hydro v/a head $dissipation (-q,*)
8241301 -1.0000 1.2360
8241302 0.0 1.3982
*hydro curve type regime
8241400 1 4
*hydro a/v head $dissipation (-q,*)
8241401 -1.0 1.2360
8241402 0.0 0.7500
*hydro curve type regime

```

```

8241500 1 5
*hydro v/a head $dissipation (-q,*)
8241501 0.0 1.0
8241502 1.0 2.0
*hydro curve type regime
8241600 1 6
*hydro a/v head
8241601 0.0 0.75
8241602 1.0 2.0
*hydro curve type regime
8241700 1 7
*hydro v/a head
8241701 -1.0 0.20
8241702 0.0 1.00
*hydro curve type regime
8241800 1 8
*hydro a/v head
8241801 -1.0 0.20
8241802 0.0 -0.30
*hydro curve type regime
8241900 1 9
*hydro v/a torque $normal (+q,*)
8241901 0.0 0.7857
8241902 0.1042 0.7698
8241903 0.2083 0.7651
8241904 0.3125 0.7651
8241905 0.4167 0.7779
8241906 0.5208 0.8016
8241907 0.6250 0.8333
8241908 0.7292 0.9048
8241909 0.8333 0.9683
8241910 0.9375 0.9971
8241911 1.0000 1.0000
*hydro curve type regime
8242000 1 10
*hydro a/v torque $normal (+q,*)
8242001 0.0000 0.1550
8242002 0.5000 0.2500
8242003 0.6250 0.3910
8242004 0.7140 0.5171
8242005 0.8000 0.6502
8242006 0.8728 0.7798
8242007 0.9600 0.9088
8242008 1.0000 1.0000
*hydro curve type regime
8242100 1 11
*hydro v/a torque $dissipation (-q,*)
8242101 -1.0 0.7
8242102 0.0 0.7857
*hydro curve type regime

```

```

8042200      2      4
*hydro      a/v      torque      $dissipation (-Q,IN)
8042201      -1.0      0.7
8042202      0.0      0.30
*
*hydro      curve type      regime
8042300      2      5
*hydro      v/s      torque
8042301      0.0      -0.60
8042302      1.0      -0.20
*
*hydro      curve type      regime
8042400      2      6
*hydro      a/v      torque
8042401      0.0      0.30
8042402      1.0      -0.20
*
*hydro      curve type      regime
8042500      2      7
*hydro      v/s      torque
8042501      -1.0      -1.40
8042502      0.0      -0.60
*
*hydro      curve type      regime
8042600      2      8
*hydro      a/v      torque
8042601      -1.0      -1.40
8042602      0.0      -0.15

```

```

*****
$condensate pump discharge piping to l.p. heater 1 $
*****
*hydro      component name      component type
8260000      'cond dis'      angivol
*****
*hydro      area      length      volume
8260101      2.4053      0.0      279.1433
*
*hydro      horz angle      vert angle      delta z
8260102      0.0      0.0      0.0
*
*hydro      roughness      hyd diam      fe
8260103      0.00015      1.75      00
*
*hydro      ic      pressure      energy      quality
8260200      0      537.48000      70.44000      1118.7000      00000000
*****
$junction connecting condensate pump discharge piping to l.p. heater 1 $
*****
*hydro      component name      component type
8280000      'jun c1'      valve
*****
*hydro      from      to      area      f loss      r loss      wchgs
8280101      826010000      826000000      2.4053      32.4193      32.4193      00100
*
*hydro      junc dia      beta      c      m
8280110      0.0      0.      1.      1.

```

```

*hydro      vel/flw      f flowrate      g flowrate      j flowrate
8280201      0      13.577000      13.577000      0.0
*
*hydro      valve type
8280300      chvly
*
*hydro      chvly type      init. posn      back press      leak ratio
8280301      0      0      0      0
*
*****
$l.p. heaters 1 and 2 - this component represents l.p. heaters 1a, 1b, 2a, and 2b. volume 1 is the 1a and 1b heaters. volume 2 is the 2a and 2b heaters.
*****
*hydro      component name      component type
8300000      'htrs 1&2'      pipe
*****
*hydro      no. volumes
8300001      2
*
*hydro      vol area
8300101      4.3474      vol 1
8300102      3.3341      2
*
*hydro      junc area
8300201      3.3341      junc 1
*
*hydro      length
8300301      0.0      vol 2
*
*hydro      volume
8300401      268.1559      vol 1
8300402      242.2777      2
*
*hydro      vert angle
8300601      0.0      vol 2
*
*hydro      roughness      hyd diam
8300801      0.000005      0.0439      vol 1
8300802      0.000005      0.0543      2
*
*hydro      fe
8301001      00      vol 2
*
*hydro      f wchgs
8301101      000100      junc 1
*
*hydro      ic      pressure      energy      quality
8301201      0      489.28000      135.03000      1118.9000      00000000      0.0
8301202      0      469.98000      169.61000      1118.9000      00000000      0.0
*
*hydro      vel/flw
8301300      0
*
*hydro      f flowrate      g flowrate      j flowrate
8301301      9.9762000      9.9762000      0.0      01
*
*hydro      junc dia      beta      c      m
8301401      0.0      0.      1.      1.
*****
$junction connecting l.p. heater 2 outlet to piping between heaters 2&3 $
*****
*hydro      component name      component type
8320000      'jun c2'      angijun

```

```
*hydro from to area f loss r loss vcrhs
#320101 #34010000 #34000000 2.5368 4.4615 4.4615 00100
```

```
*
* in dia beta c n
#320110 0.627 0.0 1. 1.
```

```
*hydro vel/flw f flowrate g flowrate j flowrate
#320201 0 13.281000 13.281000 0.0
```

```
*
* piping connecting l.p. heaters 2 and 3
```

```
*hydro component name component type
#340000 'ht2to3' angvol
```

```
*
*hydro area length volume
#340101 2.5368 0.0 420.5482
```

```
*hydro horiz angle vert angle delta z
#340102 0.0 0.0 0.0
```

```
*hydro roughness hyd diam fe
#340103 0.00015 1.2117 00
```

```
*hydro ic pressure energy quality
#340200 0 484.23000 109.84000 1118.9000 00000000
```

```
*
* junction connecting the polisher to l.p. heater 2
```

```
*hydro component name component type
#360000 'jun c3' angjun
```

```
*hydro from to area f loss r loss vcrhs
#360101 #34010000 #40000000 2.5368 0.0 0.0 00100
```

```
*
* in dia beta c n
#360110 0.627 0.0 1. 1.
```

```
*hydro vel/flw f flowrate g flowrate flowrate
#360201 0 13.282000 13.282000 0.0
```

```
*
* l.p. heaters 3,4 and 5 and piping between l.p. heater 5 and the s/w
* pump suction header. the heaters are combine as in the l.p. heaters
* 1 and 2 volume 1 represents 3a and 3b heaters, volume 2 represents 4a
* and 4b heaters, volume 3 represents 5a and 5b heaters and volume 4
* represents the piping between l.p. heaters 5 and the s/w pump suction
* header
```

```
*hydro component name component type
#400000 'lp ht3' pipe
```

```
*hydro no. volumes
#400001 4
```

```
*hydro vol area vol
#400101 3.4574 1
#400102 3.4593 2
#400103 3.5074 3
#400104 2.4053 4
```

```
*hydro length vol
#400301 0.0 4
```

```
*hydro volume vol
```

```
#400401 406.7622 1
#400402 328.0331 2
#400403 277.4071 3
#400404 276.6769 4
```

```
*hydro vert angle vol
#400601 0.0 4
```

```
*hydro roughness hyd diam vol
#400801 0.000005 0.0063 1
#400802 0.000005 0.0043 2
#400803 0.00015 0.0750 4
```

```
*hydro f loss r loss jun
#400901 0.0 0.0 0
#400902 4.0 4.0 0
```

```
*hydro fe vol
#401001 00 4
```

```
*hydro vcrhs jun
#401101 00100 3
```

```
*hydro ic pressure energy quality vol
#401201 0 440.57000 224.10000 1118.8000 00000000 0.0 01
#401202 0 416.34000 277.71000 1118.7000 00000000 0.0 02
#401203 0 398.91000 341.79000 1118.6000 00000000 0.0 03
#401204 0 384.33000 341.30000 1118.5000 00000000 0.0 04
```

```
*hydro vel/flw
#401300 0
```

```
*hydro f flowrate g flowrate j flowrate jun
#401301 0 9770000 0.977000 0.0 01
#401302 10.259000 10.259000 0.0 02
#401303 15.339000 15.339000 0.0 03
```

```
*
* in dia beta c n
#401401 0.627 0.0 1. 1.
```

```
*
* junction connecting l.p. heater 5 outlet piping to s/w pump suction
* header
```

```
*hydro component name component type
#420000 'jun c4' angjun
```

```
*hydro from to area f loss r loss vcrhs
#420101 #40010000 #54000000 2.4053 0.0 0.0 00100
```

```
*
* in dia beta c n
#420110 2.348 0.0 1. 1.
```

```
*hydro vel/flw f flowrate g flowrate j flowrate
#420201 0 15.340000 15.340000 0.0
```

```
*
* l.p. heater bypass valve (ncv-1459)
```

```
*hydro component name component type
#440000 'ncv-1459' valve
```

```
*hydro from to area f loss r loss vcrhs
#440101 #26010000 #54000000 0.3874 177.4948 177.4948 00100
```

```
*
* in dia beta c n
```



```

#440110 1.891 0.0 1. 1
*hydro vel/flow f flowrate g flowrate j flowrate
#440201 0 0000000 0000000 0.0
*hydro valve type
#440300 trpvlv
*hydro trip no.
#440301 609
*-----*
$heater drain system - drain pumps modeled as time dependent volume and
$ junction - drain pumps provide approximately 25%
$ of total feed flow.
*-----*
*hydro component name component type
#500000 'dr'inpmp' 'fedpvol'
*-----*
*hydro area length volume
#500101 0.9576 0.0 1.0e+06
*hydro horz angle vert angle delta z
#500102 0.0 0.0 0.0
*hydro roughness hyd diam fe
#500103 0.0 0.0 10
*hydro ic trip no. alpha vrc numeric vrc
#500200 01
*hydro time eq. temp quality
#500201 0.0 379.0550 0.0
*-----*
*hydro component name component type
#520000 'drainflw' 'fedjun'
*-----*
*hydro from to area
#520101 050000000 054000000 0.9576
*hydro vel/flow trip no. alpha vrc numeric vrc
#520100 1 609
*hydro time f flowrate g flowrate j flowrate
#520201 1.0 0.0 0.0 0
#520202 0.0 783.1187 0.0 0
*-----*
$main feedwater pump suction header tank
*-----*
*hydro component name component type
#540000 'pmp hdr' 'englvcl'
*-----*
*hydro area length volume
#540101 4.4969 0.0 78.6960
*hydro horz angle vert angle delta z
#540102 0.0 0.0 0.0
*hydro roughness hyd diam fe
#540103 0.00015 2.5928 00
*hydro ic pressure energy quality
#540200 0 283.50000 344.40000 1119.5000 00000000

```

```

*-----*
$junction connecting the mfw pump suction header to the mfw pump
$suction piping
*-----*
*hydro component name component type
#560000 'jun fwl' 'engljun'
*-----*
*hydro from to area f loss r loss vrate
#560101 054010000 060000000 3.9379 0.0 0.0 00100
*hydro in dia beta c w
#560110 1.726 1.
*hydro vel/flow f flowrate g flowrate j flowrate
#600201 0 13.010000 13.010000 0.0
*-----*
$mfw pump suction pipe
*-----*
*hydro component name component type
#600000 'pmp scin' 'englvcl'
*-----*
*hydro area length volume
#600101 3.9379 0.0 368.6818
*hydro horz angle vert angle delta z
#600102 0.0 0.0 0.0
*hydro roughness hyd diam fe
#600103 0.00015 1.5103 00
*hydro ic pressure energy quality
#600200 0 282.97000 344.40000 1119.5000 00000000
*-----*
$main feedwater pump a
*-----*
*hydro component name component type
#610000 'mfw pmpa' 'pump'
*-----*
*hydro area length volume
#610101 2.6802 10.4032 0.0
*hydro horz angle vert angle delta z
#610102 0.0 0.0 0.0
*hydro equil flag
#610103 60
*hydro from jun area f loss r loss vrate
#610108 060010000 1.9690 0.0 0.0 00000
*hydro to jun area f loss r loss vrate
#610109 062000000 1.6545 0.0 0.0 00000
*hydro in dia beta c w
#610110 0.0 0.0 1. 1.
#610111 0.0 0.0 1. 1.
*hydro ic pressure energy quality
#610200 0 715.73000 344.60000 1119.7000 00000000
*-----*
*hydro vel/flow f flowrate g flowrate j flowrate
#610201 0 13.017000 13.017000 0.0

```

```

*hydro vel/ftw f flowrate g flowrate j flowrate
0610202 0 15.434000 15.434000 0.0
-----*
*hydro gtd1 dfact diff i tort i pvel i frp no rvs i
061001 0 -1 0 -1 -1 0 0 0
061202 2570.0000 1.0000000 12080.000 1885.0000 0617.9318 043.0000
061003 62.400000 0.0000000 0.0000000 90.180000 0.0180000 00.000000
-----*
*hydro rated pump vel. inlt/rated vel. rated flow rated head
*hydro rated torque mom of inertia rated dens air torque
*hydro coeff. ft2 coeff. ftD coeff. ft1 coeff. ft2
*hydro curve type regime
0611100
*
*hydro v/a head $normal (+q,*)
0611101 0.0 1.2482
0611102 0.0994 1.2372
0611103 0.0788 1.2262
0611104 0.1576 1.2012
0611105 0.2364 1.185
0611106 0.3152 1.1692
0611107 0.3940 1.1532
0611108 0.4728 1.1372
0611109 0.5516 1.1211
0611110 0.6304 1.1051
0611111 0.7092 1.1111
0611112 0.7880 1.0891
0611113 0.8668 1.0631
0611114 0.9456 1.0330
0611115 1.0000 1.0000
*
*hydro curve type regime
0611200
*
*hydro a/v head $normal (+q,*)
0611201 0.0000 0.3000
0611202 0.5000 0.0120
0611203 0.6250 0.2860
0611204 0.7140 0.4220
0611205 0.7821 0.4812
0611206 0.8400 0.6191
0611207 0.9085 0.7649
0611208 0.9762 0.9286
0611209 1.0000 1.0000
*
*hydro curve type regime
0611300
*
*hydro v/a head $dissipation (-q,*)
0611301 -1.0000 1.2360
0611302 0.0 1.2482
*
*hydro curve type regime
0611400
*
*hydro a/v head $dissipation (-q,*)
0611401 -1.0 1.2380
0611402 0.0 0.7500
*
*hydro curve type regime

```

```

0611500 1 5
*
*hydro v/a head $dissipation (-q,*)
0611501 0.0 1.0
0611502 1.0 2.0
*
*hydro curve type regime
0611600
*
*hydro a/v head
0611601 0.0 0.75
0611602 1.0 2.0
*
*hydro curve type regime
0611700
*
*hydro v/a head
0611701 -1.0 0.20
0611702 0.0 1.00
*
*hydro curve type regime
0611800
*
*hydro a/v head
0611801 -1.0 0.20
0611802 0.0 0.50
*
*hydro curve type regime
0611900
*
*hydro v/a torque $normal (+q,*)
0611901 0.0 0.5321
0611902 0.0994 0.5138
0611903 0.0788 0.5138
0611904 0.1576 0.5321
0611905 0.2364 0.5488
0611906 0.3152 0.6239
0611907 0.3940 0.6897
0611908 0.4728 0.7248
0611909 0.5516 0.7798
0611910 0.6304 0.8277
0611911 0.7092 0.8807
0611912 0.7880 0.9174
0611913 0.8668 0.9481
0611914 0.9456 0.9808
0611915 1.0000 1.0000
*
*hydro curve type regime
0612000
*
*hydro a/v torque $normal (+q,*)
0612001 0.0000 -0.1500
0612002 0.5000 0.2500
0612003 0.6250 0.3910
0612004 0.7140 0.5100
0612005 0.7821 0.6580
0612006 0.8400 0.7420
0612007 0.9085 0.8443
0612008 0.9762 0.9177
0612009 1.0000 1.0000
*
*hydro curve type regime
0612100
*

```

```

*hydro v/a torque $dissipation (-q,wh)
0612101 -1.0 0.7
0612102 0.0 0.7321
*
*hydro curve type regime
0612200 2 8
*
*hydro v/a torque $dissipation (-q,wh)
0612301 1.0 0.7
0612302 0.0 0.3
*
*hydro curve type regime
0612300 2 8
*
*hydro v/a torque
0612301 1.0 -0.80
0612302 1.0 -0.20
*
*hydro curve type regime
0612400 2 8
*
*hydro v/a torque
0612401 0.0 0.3
0612402 1.0 -0.20
*
*hydro curve type regime
0612500 2 8
*
*hydro v/a torque
0612501 -1.0 -1.80
0612502 0.0 -0.80
*
*hydro curve type regime
0612600 2 8
*
*hydro v/a torque
0612601 -1.0 -1.80
0612602 1.0 -0.15
*

```

```

$-----$
$SAFE pump & discharge piping and check valve $
$-----$
*hydro component name component type
0620000 "SAFE DIS" "chkvly"
$-----$
*hydro area length volume
0620101 1.2500 50.0 3.0
*
*hydro horiz angle vert angle delta z
0620102 0.0 0.0 0.0
*
*hydro roughness hyd diam fa
0620103 0.00015 1.4000 00
*
*hydro ic pressure energy quality
0620200 0 1047.3000 344.8700 1703.0000 00000000
*
$-----$
$SAFE pump & discharge piping check valve $
$-----$
*hydro component name component type
0630000 "SAFE DIS" "chkvly"

```

```

$-----$
*hydro from to area f loss r loss vcats
0630101 062010000 063000300 1.0500 0.0 0.0 00100
*
*hydro junc dia beta c k
0630110 0.0 0. 1. 1.
*
*hydro vel/flow f flowrate g flowrate j flowrate
0630201 0 15.412000 15.412000 0.0
*
*hydro valve type
0630300 "chkvly"
*
*hydro chkvly type init postn back press leak vcatp
0630301 0 0 0 0 0
*

```

```

$-----$
$SAFE in feedwater pump b $
$-----$
*hydro component name component type
0640000 "SAFE PMP" "pump"
$-----$
*hydro area length volume
0640101 2.5802 10.4332 0.0
*
*hydro horiz angle vert angle delta z
0640102 0.0 0.0 0.0
*
*hydro equil flag
0640103 00
*
*hydro from junc area f loss r loss vcats
0640108 060010000 1.8500 0.0 0.0 00000
*
*hydro to junc area f loss r loss vcats
0640109 060000000 1.8500 0.0 0.0 00000
*
*hydro junc dia beta c k
0640110 0.0 0. 1. 1.
0640111 0.0 0. 1. 1.
*
*hydro ic pressure energy quality
0640200 0 715.73000 344.00000 1116.7000 00000000
$-----$
*hydro vel/flow f flowrate g flowrate j flowrate
0640201 0 12.017000 12.017000 0.0
$-----$
*hydro vel/flow f flowrate g flowrate j flowrate
0640202 0 15.434000 15.434000 0.0
$-----$
*hydro ptdi pfact diff z fork i pvel j trip no rvrs i
0640301 0 -1 0 -1 -1 0.29 0 0
0640302 3070.0000 1.0000000 12500.000 1685.0000 0017.0010 1843.0000
0640303 62.405000 0.0000000 0.0000000 60.180000 0.0180000 00000000
$-----$
*hydro rated pump vel. init/rated vel. rated flow rated head
*
*hydro rated torque mom of inertia rated dens str torque
*
*hydro coeff. t12 coeff. t10 coeff. t11 coeff. t13
*
*hydro curve type regime
0641100 1
*
*hydro v/a head $storm1 (-q,wh)
0641101 0.0 1.450

```

```

8041102 0.0394 1.2372
8041103 0.0788 1.2762
8041104 0.1576 1.3152
8041105 0.2364 1.3542
8041106 0.3152 1.3932
8041107 0.3940 1.4322
8041108 0.4728 1.4712
8041109 0.5516 1.5102
8041110 0.6304 1.5492
8041111 0.7092 1.5882
8041112 0.7880 1.6272
8041113 0.8668 1.6662
8041114 0.9456 1.7052
8041115 1.0244 1.7442
*
*hydro curve type regime
8041200 1 $normal (+q,+h)
*
*hydro s/v head
8041201 0.0000 0.3000
8041202 0.5000 0.0000
8041203 0.6750 0.2800
8041204 0.7400 0.4200
8041205 0.7931 0.4917
8041206 0.8400 0.6191
8041207 0.9005 0.7649
8041208 0.9762 0.9388
8041209 1.0700 1.0000
*
*hydro curve type regime
8041300 1
*
*hydro v/a head $dissipation (-q,+h)
8041301 -1.0000 1.7360
8041302 0.0 1.2862
*
*hydro curve type regime
8041400 1
*
*hydro s/v head $dissipation (-q,+h)
8041401 -1.0 1.2360
8041402 0.0 0.7500
*
*hydro curve type regime
8041500 1
*
*hydro v/a head $dissipation (-q,+h)
8041501 0.0 1.0
8041502 -1.0 2.0
*
*hydro curve type regime
8041600 1
*
*hydro s/v head
8041601 0.0 0.75
8041602 1.0 2.0
*
*hydro curve type regime
8041700 1
*
*hydro v/a head
8041701 -1.0 0.20
8041702 0.0 1.00

```

```

*
*hydro curve type regime
8041800 1
*
*hydro s/v head
8041801 -1.0 0.20
8041802 0.0 0.30
*
*hydro curve type regime
8041900 2
*
*hydro v/a torque $normal (+q,+h)
8041901 0.0 0.5321
8041902 0.0394 0.5138
8041903 0.0788 0.5138
8041904 0.1576 0.5321
8041905 0.2364 0.5609
8041906 0.3152 0.6239
8041907 0.3940 0.6907
8041908 0.4728 0.7240
8041909 0.5516 0.7799
8041910 0.6304 0.8257
8041911 0.7092 0.8907
8041912 0.7880 0.9174
8041913 0.8668 0.9541
8041914 0.9456 0.9902
8041915 1.0244 1.0000
*
*hydro curve type regime
8042000 2
*
*hydro s/v torque $normal (+q,+h)
8042001 0.0000 0.1500
8042002 0.5000 0.2500
8042003 0.6750 0.3910
8042004 0.7140 0.5100
8042005 0.7931 0.6040
8042006 0.8400 0.7420
8042007 0.9005 0.8442
8042008 0.9762 0.9612
8042009 1.0000 1.0000
*
*hydro curve type regime
8042100 2
*
*hydro v/a torque $dissipation (-q,+h)
8042101 1.0 0.7
8042102 0.0 0.5321
*
*hydro curve type regime
8042200 2
*
*hydro s/v torque $dissipation (-q,+h)
8042201 -1.0 0.7
8042202 0.0 0.3
*
*hydro curve type regime
8042300 2
*
*hydro v/a torque
8042301 0.0 -0.60
8042302 1.0 -0.20
*
*hydro curve type regime

```

```

*662400      2      8
*hydro
662401      0.0      torque
662402      1.0      -0.20
*
*hydro      curve type      regime
662500      2
*
*hydro      0.0      torque
662501      1.0      -1.40
662502      0.0      -0.60
*
*hydro      curve type      regime
662600      2
*
*hydro      0.0      torque
662601      1.0      -1.40
662602      0.0      -0.15

```

```

$*****
$sew pump b discharge piping and check valve $

```

```

*hydro      component name      component type
665000      'pmp dis'      'anglval'
*
*hydro      area      length      volume
6650101      1.6585      50.0      8.0
*
*hydro      horz angle      vert angle      delta z
6650102      0.0      0.0      0.0
*
*hydro      roughness      hyd diam      fe
6650103      0.00015      1.4532      00
*
*hydro      ic      pressure      energy      quality
6650200      0      1047.3000      344.60000      1109.0000      00000000

```

```

$*****
$sew pump b discharge piping check valve $

```

```

*hydro      component name      component type
666000      'sw'val'      'valve'
*
*hydro      from      to      area      f loss      r loss      vcats
6660101      66510000      66700000      1.0585      0.0      0.0      00100
*
*hydro      junc dia      beta      c      m
6660110      0.0      0      1      1
*
*hydro      vel/flw      f flowrate      g flowrate      j flowrate
6660201      0      15.412000      15.412000      0.0
*
*hydro      valve type
6660300      'chkv'
*
*hydro      chkvly type      init      posn      back press      leak ratio
6660301      0      0      0      0

```

```

$*****
$sew pump discharge pipe - combined piping $

```

```

*hydro      component name      component type
667000      'pmp disc'      'anglval'

```

```

*hydro      area      length      volume
6670101      2.2170      0.0      152.2160
*
*hydro      horz angle      vert angle      delta z
6670102      0.0      0.0      0.0
*
*hydro      roughness      hyd diam      fe
6670103      0.00015      1.4532      00
*
*hydro      ic      pressure      energy      quality
6670200      0      1046.7000      344.60000      1109.1000      00000000

```

```

$*****
$main freshwater pump recirculation line - models both a and b lines $

```

```

*hydro      component name      component type
668000      'fw pmp'      'pmp'
*
*hydro      from      to      area
6680101      66701000      67000000      0.1705
*
*hydro      vel/flw      trip no.      alpha vrc      numeric vrc
6680200      0      0      'ctrlv'      0.40
*
*hydro      ctrlvly      f flowrate      g flowrate      j flowrate
6680201      0.0      0.0      0.0      0
6680202      2000.0      2000.0      -570.0      0

```

```

$*****
$sew line $

```

```

*hydro      component name      component type
670000      'sew line'      'anglval'
*
*hydro      area      length      volume
6700101      1.0e+06      0.0      1.0e+06
*
*hydro      horz angle      vert angle      delta z
6700102      0.0      0.0      0.0
*
*hydro      roughness      hyd diam      fe
6700103      0.0      0.0      10
*
*hydro      ic      trip no.      alpha vrc      numeric vrc
6700200      00
*
*hydro      time      pressure      quality
6700201      6.0      1.5      0.0

```

```

$*****
$junction connecting the pump discharge to a heater $

```

```

*hydro      component name      component type
672000      'jvn fwt'      'jvn'
*
*hydro      from      to      area      f loss      r loss      vcats
6720101      66701000      67400000      2.3131      1.0      0.0      30100
*
*hydro      junc dia      beta      c      m
6720110      0.0      0.0      1      1
*
*hydro      vel/flw      f flowrate      g flowrate      j flowrate
6720201      0      15.412000      15.412000      0.0

```

```

$*****
$high pressure feedwater heaters 6a and 6b $

```



```

*hydro component name component type
E740000 h.p. htr angivol
*
*hydro area length volume
E740101 5.7289 0.0 401.0188
*
*hydro horz angle vert angle delta z
E740102 0.0 0.0 0.0
*
*hydro roughness hyd diam fe
E740103 0.00008 0.0403 00
*

```

```

*hydro ic pressure energy quality
E740200 0 1024.0000 417.4000 1109.7000 .00000000
*
junction connecting h.p. heater to h.p. heater outlet piping
*

```

```

*hydro component name component type
E760000 'jun fa3' angivol
*
*hydro from to area f loss r loss vchgs
E760101 E74010000 0780000000 3.2170 7.0710 2.0710 30100
*
*hydro jun dia beta c s
E760110 0.0 0. 1. 1.
*

```

```

*hydro vel/fw f flowrate g flowrate l flowrate
E760201 0 16.254000 16.254000 0.0
*
h.p. heater outlet piping and main feedwater header
*

```

```

*hydro component name component type
E780000 'afa hdr' angivol
*
*hydro area length volume
E780101 3.2170 0.0 117.4790
*
*hydro horz angle vert angle delta z
E780102 0.0 0.0 0.0
*
*hydro roughness hyd diam fe
E780103 0.00018 1.4532 00
*

```

```

*hydro ic pressure energy quality
E780200 0 1024.0000 417.4000 1109.7000 .00000000
*
the following input represents the ecch system including the
$ accumulators, hpl, lps, and makeup systems
*

```

```

*hydro component name component type
E110000 'accum100' accum
*
*hydro area length volume
E110101 0. 15.73 1200.
*
*hydro horz angle vert angle delta z
E110102 0. -90. -15.73
*
*hydro roughness hyd diam fe
E110103 .00015 0. 00
*

```

```

*hydro pressure temperature

```

```

E110200 0.75 80.
*
*hydro to area f loss r loss vchgs
E111101 021000000 0.3941 1.12 1.63 00000
*
*hydro lig l1g line elev well htr well well n2
*
*hydro vol l1l length drop thck f1g dens hcap tcon
E112200 023. 0. 28.70 -6.967 0.174 0 0 0 0
*

```

```

*hydro component name component type
E120000 'accum100' accum
*
*hydro area length volume
E120101 0. 15.73 1200.
*
*hydro horz angle vert angle delta z
E120102 0. -90. -15.73
*
*hydro roughness hyd diam fe
E120103 .00015 0. 00
*

```

```

*hydro pressure temperature
E120200 0.75 80.
*

```

```

*hydro to area f loss r loss vchgs
E121101 022000000 0.3941 1.4 1.9 00000
*
*hydro lig l1g line elev well htr well well n2
*
*hydro vol l1l length drop thck f1g dens hcap tcon
E122200 023. 0. 40.42 -1.890 0.174 0 0 0 0
*

```

```

*hydro component name component type
E130000 'accum100' accum
*
*hydro area length volume
E130101 0. 15.73 1200.
*
*hydro horz angle vert angle delta z
E130102 0. -90. -15.73
*
*hydro roughness hyd diam fe
E130103 .00015 0. 00
*

```

```

*hydro pressure temperature
E130200 0.75 80.
*

```

```

*hydro to area f loss r loss vchgs
E121101 023000000 0.3941 0.98 1.36 00000
*
*hydro lig l1g line elev well htr well well n2
*
*hydro vol l1l length drop thck f1g dens hcap tcon
E132200 023. 0. 15.981 -11.267 0.174 0 0 0 0
*

```

```

*hydro component name component type
E210000 'eccoline' angivol
*
*hydro area length volume
E210101 .3041 56.728 0.
*
*hydro horz angle vert angle delta z
E210102 0. 0. 4.66
*
*hydro roughness hyd diam fe
E210103 .00015 0. 00
*

```

```

*
*hydro ic pressure eq temp
9210200 0 2304.0000 114.0000 1048.0000 00000000
*-----*
*hydro component name component type
9210000 'eccaline' 'mg/vol'
*-----*
*hydro area length volume
9220101 0.2041 25.30 0.
*
*hydro horz angle vert angle delta z
9220102 0. -3. -1.25
*
*hydro roughness hyd diam fe
9230103 0.015 0. 00
*
*hydro ic pressure eq temp
9230200 0 2303.0000 114.21000 1048.0000 00000000
*-----*
*hydro component name component type
9230000 'eccaline' 'mg/vol'
*-----*
*hydro area length volume
9230101 0.2041 25.30 0.
*
*hydro horz angle vert angle delta z
9230102 0. 0. 8.95
*
*hydro roughness hyd diam fe
9230103 0.015 0. 00
*
*hydro ic pressure eq temp
9210200 0 2303.0000 114.89000 1048.0000 00000000
*-----*
*hydro component name component type
9210000 'ipisourc' 'mg/vol'
*-----*
*hydro area length volume
9210101 1.0e6 0.0 1.0e+06
*
*hydro horz angle vert angle delta z
9210102 0.0 0.0 0.0
*
*hydro roughness hyd diam fe
9210103 0.0 0.0 10
*
*hydro ic trip no. alpha vrc numeric vrc
9310200 03
*
*hydro time pressure eq temp
9310201 0 144 90
*-----*
*hydro component name component type
9320000 'ipisourc' 'mg/vol'
*-----*
*hydro area length volume
9320101 1.0e6 0.0 1.0e+06
*
*hydro horz angle vert angle delta z
9320102 0.0 0.0 0.0
*
*hydro roughness hyd diam fe
9320103 0.0 0.0 10

```

```

*
*hydro ic trip no. alpha vrc numeric vrc
9320200 03
*
*hydro time pressure eq temp
9320201 0 144 90
*-----*
*hydro component name component type
9330000 'ipisourc' 'mg/vol'
*-----*
*hydro area length volume
9330101 1.0e6 0.0 1.0e+06
*
*hydro horz angle vert angle delta z
9330102 0.0 0.0 0.0
*
*hydro roughness hyd diam fe
9330103 0.0 0.0 10
*
*hydro ic trip no. alpha vrc numeric vrc
9330200 03
*
*hydro time pressure eq temp
9330201 0 144 90
*-----*
*hydro component name component type
9410000 'ipic11' 'mg/vol'
*-----*
*hydro from to area
9410101 921000000 921000000 2532
*
*hydro vel/ftw trip no. alpha vrc numeric vrc
9410200 0 608 0 921010000
*
*hydro p f velocity g velocity j velocity
9410201 -1.0e99 0. 0. 0.
9410202 0. 0. 0. 0.
9410203 1. 32.26 0. 0.
9410204 68.17 32.26 0. 0.
9410205 97.23 26.39 0. 0.
9410206 127.4 17.0 0. 0.
9410207 144.7 0. 0. 0.
9410208 3000. 0. 0. 0.
*-----*
*hydro component name component type
9420000 'ipic12' 'mg/vol'
*-----*
*hydro from to area
9420101 932000000 932000000 2532
*
*hydro vel/ftw trip no. alpha vrc numeric vrc
9420200 0 608 0 932010000
*
*hydro p f velocity g velocity j velocity
9420201 -1.0e99 0. 0. 0.
9420202 0. 0. 0. 0.
9420203 1. 32.26 0. 0.
9420204 68.17 32.26 0. 0.
9420205 97.23 26.39 0. 0.
9420206 127.4 17.0 0. 0.
9420207 144.7 0. 0. 0.
9420208 3000. 0. 0. 0.
*-----*
*hydro component name component type

```

```

9430000 'tpjct1' tmdpjun
*
*hydro from to area
9430101 033000000 923000000 .2532
*
*hydro vel/flw trip no. alpha vrc numeric vrc
9430200 0 668 p 923010000
*
*hydro p f velocity g velocity j velocity
9430201 -1.0e99 0 0 0
9430202 0 0 0 0
9430203 15 22.28 0 0
9430204 69.17 32.28 0 0
9430205 97.23 28.35 0 0
9430206 127.4 17.60 0 0
9430207 144.7 0 0 0
9430208 2000 0 0 0
*
*hydro component name component type
9510000 'tpjct1' tmdpvol
*
*hydro area length volume
9510101 1.0e6 0.0 1.0e+06
*
*hydro horz angle vert angle delta z
9510102 0.0 0.0 0.0
*
*hydro roughness hyd diam fe
9510103 0.0 0.0 10
*
*hydro ic trip no. alpha vrc numeric vrc
9510200 03
*
*hydro time pressure eq temp
9510201 0 1000 90
*
*hydro component name component type
9520000 'tpjct1' tmdpvol
*
*hydro area length volume
9520101 1.0e6 0.0 1.0e+06
*
*hydro horz angle vert angle delta z
9520102 0.0 0.0 0.0
*
*hydro roughness hyd diam fe
9520103 0.0 0.0 10
*
*hydro ic trip no. alpha vrc numeric vrc
9520200 03
*
*hydro time pressure eq temp
9520201 0 1000 90
*
*hydro component name component type
9530000 'tpjct1' tmdpvol
*
*hydro area length volume
9530101 1.0e6 0.0 1.0e+06
*
*hydro horz angle vert angle delta z
9530102 0.0 0.0 0.0

```

```

*hydro roughness h. diam fe
9530103 0.0 0.0 10
*
*hydro ic trip no. alpha vrc numeric vrc
9530200 03
*
*hydro time pressure eq temp
9530201 0 1000 90
*
*hydro component name component type
9510000 'tpjct1' tmdpjun
*
*hydro from to area
9510101 951000000 218000000 .01552
*
*hydro vel/flw trip no. alpha vrc numeric vrc
9510200 0 668 p 218010000
*
*hydro p f velocity g velocity j velocity
9510201 -1.0e99 0 0 0
9510202 0 0 0 0
9510203 15 50.40 0 0
9510204 615. 36.45 0 0
9510205 1015. 27.72 0 0
9510206 1205. 19.57 0 0
9510207 1415. 8.932 0 0
9510208 1470. 0 0 0
9510209 2000. 0 0 0
*
*hydro component name component type
9520000 'tpjct1' tmdpjun
*
*hydro from to area
9520101 952000000 218000000 .01552
*
*hydro vel/flw trip no. alpha vrc numeric vrc
9520200 0 668 p 218010000
*
*hydro p f velocity g velocity j velocity
9520201 -1.0e99 0 0 0
9520202 0 0 0 0
9520203 15 50.40 0 0
9520204 615. 36.45 0 0
9520205 1015. 27.72 0 0
9520206 1205. 19.57 0 0
9520207 1415. 8.932 0 0
9520208 1470. 0 0 0
9520209 2000. 0 0 0
*
*hydro component name component type
9530000 'tpjct1' tmdpjun
*
*hydro from to area
9530101 953000000 218000000 .01552
*
*hydro vel/flw trip no. alpha vrc numeric vrc
9530200 0 668 p 218010000
*
*hydro p f velocity g velocity j velocity
9530201 -1.0e99 0 0 0
9530202 0 0 0 0
9530203 15 50.40 0 0
9530204 615. 36.45 0 0
9530205 1015. 27.72 0 0

```

```

9630206 1296.      19.57      0.      0
9630207 1415.      6.832      0.      0
9630208 1470.      0.      0.      0
9630209 3000.      0.      0.      0
*****
*hydro component name component type
*hydro
*hydro000
-----
*hydro area length volume
*hydro001
1.0e6 0.0 1.0e+06
*
*hydro horz angle vert angle delta z
*hydro002
0.0 0.0 0.0
*
*hydro roughness hyd diam fe
*hydro003
0.0 0.0 10
*
*hydro ic trip no. alpha vrc numeric vrc
*hydro004
03 000
*
*hydro time pressure eq temp
*hydro005
1.0e6 2250 493
*hydro006
0. 2250 493
*hydro007
291. 2250 493
*hydro008
301. 2250 125
*hydro009
874. 2250 125
*hydro010
884. 2250 90
*hydro011
1.0e6 2250 90
*****
*hydro component name component type
*hydro
*hydro000
'makeup' 'makeup'
-----
*hydro from to area
*hydro001
971000000 318700000 0.3755
*
*hydro vel/flw trip no. alpha vrc numeric vrc
*hydro002
0 0
*
*hydro ctrl/val f velocity g velocity j velocity
*hydro003
-69. -4.994 0. 0
*hydro004
0. 0 0. 0
*hydro005
154. 0.137 0. 0
*
$*****
$constant pressure volume for steady state initialization only!
$*****
*hydro component name component type
*hydro
*hydro000
'const p' 'indpvol'
-----
*hydro area length volume
*hydro001
1.0e6 0.0 1.0e+06
*
*hydro horz angle vert angle delta z
*hydro002
0.0 0.0 0.0
*
*hydro roughness hyd diam fe
*hydro003
0.0 0.0 10
*
*hydro ic trip no. alpha vrc numeric vrc
*hydro004
02 0
*
*hydro time pressure quality
*hydro005
0.0 2250.0 1.0

```

```

$*****
*hydro component name component type
*hydro
*hydro000
'const ju' 'shljun'
-----
*hydro from to area f loss r loss vcont
*hydro001
098000000 340000000 25.056 0.0 0.0 30000
*
*hydro vel/flw f flowrate g flowrate j flowrate
*hydro002
0.0 0.0 0.0
$*****
$
$ heat structures
$
$*****
* vessel heat structures
*
* heat structure 100:
* the following data represent the vessel wall in the inlet
* annulus region
$*****
*crdno heat strc mesh pts geometry icrt flag icf coord
*crdno001
5 6 2 1 0.497
*
*crdno mesh icon flag mesh fct flag
*crdno002
0 1
*
*crdno no. intervals i. coord
*crdno003
2 6.516
*crdno004
3 7.451
*
*crdno comp no. interval no.
*crdno005
1 6
*crdno006
2 6
*
*crdno source value mesh int. no.
*crdno007
0.0 5
*
*crdno temperature mesh pt no.
*crdno008
547.45 6
*
*crdno left volume incr b.coord sa code area/factor ht str no.
*crdno009
100010000 0 1 1 2.361 1
*crdno010
100020000 0 1 1 1.785 2
*crdno011
100030000 0 1 1 1.576 3
*crdno012
100040000 0 1 1 1.576 4
*crdno013
100050000 0 1 1 2.369 5
*
*crdno ri volume incr b.coord sa code area/factor ht str no.
*crdno014
0 0 0 1 2.361 1
*crdno015
0 0 0 1 1.785 2
*crdno016
0 0 0 1 1.576 3
*crdno017
0 0 0 1 1.576 4
*crdno018
0 0 0 1 2.369 5
*
*crdno s. type s. unit left heat right heat ht str no
*crdno019
0 0.0 0.0 0.0 0.0 5
*
*crdno emiss diam heated len's grid len's gr d cf's of ht str no.
*crdno020
1 738 95.0 95.0 0.0 0.0 0.0 0.0 1.0 1
*crdno021
2 827 95.0 95.0 0.0 0.0 0.0 0.0 1.0 2

```

11001003 2.648 99.0 99.0 0.0 0.0 0.0 0.0 1.0 0  
11001004 2.648 99.0 99.0 0.0 0.0 0.0 0.0 1.0 4  
11001005 2.231 99.0 99.0 0.0 0.0 0.0 0.0 1.0 5

\* heat structure 100:  
\* the following data represent the vessel wall in the  
\* noncopper region

\*crdno heat str's mesh pts geometry init flag left coord  
11001000 7 6 2 1 0.476

\*crdno mesh join flag mesh fat flag  
11001100 0 1

\*crdno no. intervals r1 coord  
11001101 2 6.437  
11001102 3 7.282

\*crdno comp no. interval no.  
11001201 1 2  
11001202 2 3

\*crdno source value mesh int. no.  
11001301 0.0 5

\*crdno temperature mesh pt no.  
11001401 549.02 6

\*crdno left volume incr b.cond sa code area/factor ht str no.  
11001501 10601000 0 1 1 2.1110 1  
11001502 10602000 0 1 1 2.1110 2  
11001503 10603000 0 1 1 2.1110 3  
11001504 10604000 0 1 1 2.111 4  
11001505 10605000 0 1 1 2.1110 5  
11001506 10606000 0 1 1 2.1110 6  
11001507 10607000 0 1 1 4.0940 7

\*crdno r1 volume incr b.cond sa code area/factor ht str no.  
11001601 0 0 0 1 1 2.1110 1  
11001602 0 0 0 1 1 2.1110 2  
11001603 0 0 0 1 1 2.1110 3  
11001604 0 0 0 1 1 2.1110 4  
11001605 0 0 0 1 1 2.1110 5  
11001606 0 0 0 1 1 2.1110 6  
11001607 0 0 0 1 1 4.0940 7

\*crdno s. type s. mult left heat right heat ht str no.  
11001701 0 0.0 0.0 0.0 0.0 7

\*crdno equiv diam heated len's grid len's grid cf's of ht str no.  
11001801 1.925 99.0 99.0 0.0 0.0 0.0 0.0 1.0 6  
11001802 2.470 99.0 99.0 0.0 0.0 0.0 0.0 1.0 7

\* heat structure 100:  
\* the following data represent the vessel wall in the lower

\* plenum region

\*crdno heat str's mesh pts geometry init flag left coord  
11001000 1 6 2 1 0.648

\*crdno mesh join flag mesh fat flag  
11001100 0 1

\*crdno no. intervals r1 coord  
11001101 2 6.667  
11001102 3 7.099

\*crdno comp no. interval no.  
11001201 1 2  
11001202 2 3

\*crdno source value mesh int. no.  
11001301 0.0 5

\*crdno temperature mesh pt no.  
11001401 548.21 6

\*crdno left volume incr b.cond sa code area/factor ht str no.  
11001501 11001000 0 1 1 0.434 1

\*crdno r1 volume incr b.cond sa code area/factor ht str no.  
11001601 0 0 0 1 1 0.434 1

\*crdno s. type s. mult left heat right heat ht str no.  
11001701 0 0.0 0.0 0.0 0.0 1

\*crdno equiv diam heated len's grid len's grid cf's of ht str no.  
11001801 0.0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1

\* heat structure 101:  
\* the following input represents the  
\* vessel thermal shield

\*crdno heat str's mesh pts geometry init flag left coord  
11011000 8 3 2 1 5.943

\*crdno mesh join flag mesh fat flag  
11011100 0 1

\*crdno no. intervals r1 coord  
11011101 2 6.192

\*crdno comp no. interval no.  
11011201 1 2

\*crdno source value mesh int. no.  
11011301 0.0 2

\*crdno temperature mesh pt no.  
11011401 549.74 3



```

*crdno left volume incr b.cond sa code area/factor ht str no.
11011501 104010000 0 1 1 1.205 1
11011502 106010000 10000 1 1 2.111 7
11011503 106070000 0 1 1 1.488 8
*
*crdno r1 volume incr b.cond sa code area/factor ht str no.
11011601 104010000 0 1 1 1.205 1
11011602 106010000 1.000 1 1 2.111 7
11011603 106070000 0 1 1 1.488 8
*
*crdno s. type s. mult left heat right heat ht str no.
11011701 0 0.0 0.0 0.0 8
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
11011801 2.098 99.0 99.0 0.0 0.0 0.0 0.0 1.0 7
11011802 2.682 99.0 99.0 0.0 0.0 0.0 0.0 1.0 8
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
11011901 2.017 99.0 99.0 0.0 0.0 0.0 0.0 1.0 7
11011902 2.088 99.0 99.0 0.0 0.0 0.0 0.0 1.0 8
*
**101
*
* heat structure 121:
* the following data represent the core barrel wall
*
*crdno heat str's mesh pts geometry init flag left coord
11021000 12 3 2 1 5.578
*
*crdno mesh locn flag mesh fnt flag
11021100 0 1
*
*crdno no. intervals r1 coord
11021101 2 5.747
*
*crdno comp no. interval no.
11021201 1 2
*
*crdno source value mesh int. no.
11021301 0.0 2
*
*crdno temperature mesh pt no.
11021401 549.57 3
*
*crdno left volume incr b.cond sa code area/factor ht str no.
11021501 112010000 0 1 1 4.094 1
11021502 118000000 -10000 1 1 2.111 7
11021503 118010000 0 1 1 2.441 8
11021504 120010000 0 1 1 1.434 9
11021505 122000000 0 1 1 1.434 10
11021506 122020000 0 1 1 1.824 11
11021507 122010000 0 1 1 3.435 12
*
*crdno r1 volume incr b.cond sa code area/factor ht str no.
11021601 106070000 0 1 1 4.094 1
11021602 106000000 -10000 1 1 2.111 7
11021603 104010000 0 1 1 2.441 8
11021604 102010000 0 1 1 1.434 9
11021605 100010000 0 1 1 1.434 10
11021606 100020000 0 1 1 1.824 11
11021607 100000000 0 1 1 3.435 12
*
*crdno s. type s. mult left heat right heat ht str no.

```

```

11021701 0 0.0 0.0 0.0 12
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
11021801 0.573 99.0 99.0 0.0 0.0 0.0 0.0 1.0 7
11021802 1.782 99.0 99.0 0.0 0.0 0.0 0.0 1.0 7
11021803 8.055 99.0 99.0 0.0 0.0 0.0 0.0 1.0 8
11021804 9.762 99.0 99.0 0.0 0.0 0.0 0.0 1.0 9
11021805 9.762 99.0 99.0 0.0 0.0 0.0 0.0 1.0 12
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
11021901 2.794 99.0 99.0 0.0 0.0 0.0 0.0 1.0 7
11021902 2.170 99.0 99.0 0.0 0.0 0.0 0.0 1.0 2
11021903 2.170 99.0 99.0 0.0 0.0 0.0 0.0 1.0 6
11021904 0.170 99.0 99.0 0.0 0.0 0.0 0.0 1.0 7
11021905 0.813 99.0 99.0 0.0 0.0 0.0 0.0 1.0 6
11021906 0.880 99.0 99.0 0.0 0.0 0.0 0.0 1.0 9
11021907 2.880 99.0 99.0 0.0 0.0 0.0 0.0 1.0 10
11021908 3.195 99.0 99.0 0.0 0.0 0.0 0.0 1.0 11
11021909 1.965 99.0 99.0 0.0 0.0 0.0 0.0 1.0 12
*

```

```

**122
*
* heat structure 123:
* the following input represent the uh support plate
*
*crdno heat str's mesh pts geometry init flag left coord
11231000 1 3 1 1 0.0
*
*crdno mesh locn flag mesh fnt flag
11231100 0 1
*
*crdno no. intervals r1 coord
11231101 2 0.974
*
*crdno comp no. interval no.
11231201 1 2
*
*crdno source value mesh int. no.
11231301 0.0 2
*
*crdno temperature mesh pt no.
11231401 601.31 3
*
*crdno left volume incr b.cond sa code area/factor ht str no.
11231501 122010000 0 1 1 140.202 1
*
*crdno r1 volume incr b.cond sa code area/factor ht str no.
11231601 126010000 0 1 1 149.202 1
*
*crdno s. type s. mult left heat right heat ht str no.
11231701 0 0.0 0.0 0.0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
11231801 0.0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
11231901 0.0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
**123
*
* heat structure 125:
* the following ht represents the uh vertical structures
*

```

```

*crdno heat str's mesh pts geometry init flag left coord
11251000 1 3 1 1 0.164
*
*crdno mesh locn flag mesh fwt flag
11251100 0 1
*
*crdno no. intervals rt. coord
11251101 2 0.185
*
*crdno comp no. interval no.
11251201 1 2
*
*crdno source value mesh int. no.
11251301 0.0 2
*
*crdno temperature mesh pt no.
11251401 601.75 3
*
*crdno left volume incr b.cond sa code area/factor ht str no.
11251501 0 0 0 1 369.675 1
*
*crdno rt volume incr b.cond sa code area/factor ht str no.
11251601 126010000 0 1 1 369.675 1
*
*crdno s. type s. mult left heat right heat ht str no.
11251701 0 0.0 0.0 0.0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
11251801 0.0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
11251901 0.0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
* heat structure 128:
* the following data represent the vessel closure head *
*
*crdno heat str's mesh pts geometry init flag left coord
11281000 1 6 1 1 6.221
*
*crdno mesh locn flag mesh fwt flag
11281100 0 1
*
*crdno no. intervals rt. coord
11281101 2 6.240
11281102 3 7.259
*
*crdno comp no. interval no.
11281201 1 2
11281202 2 5
*
*crdno source value mesh int. no.
11281301 0.0 5
*
*crdno temperature mesh pt no.
11281401 597.53 6
*
*crdno left volume incr b.cond sa code area/factor ht str no.
11281501 126010000 0 1 1 0.540 1
*
*crdno rt volume incr b.cond sa code area/factor ht str no.
11281601 0 0 0 1 0.540 1
*

```

```

*crdno s. type s. mult left heat right heat ht str no.
11281701 0 0.0 0.0 0.0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
11281801 0.0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
11281901 0.0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
* heat structure 121:
* the following input represents the up vertical internals *
*
*crdno heat str's mesh pts geometry init flag left coord
11211000 6 3 2 1 0.257
*
*crdno mesh locn flag mesh fwt flag
11211100 0 1
*
*crdno no. intervals rt. coord
11211101 2 0.296
*
*crdno comp no. interval no.
11211201 1 2
*
*crdno source value mesh int. no.
11211301 0.0 2
*
*crdno temperature mesh pt no.
11211401 601.26 3
*
*crdno left volume incr b.cond sa code area/factor ht str no.
11211501 122010000 0 1 1 339.560 1
11211502 122020000 0 1 1 391.285 2
11211503 122030000 0 1 1 178.821 3
11211504 122040000 0 1 1 178.821 4
11211505 118010000 0 1 1 212.368 5
*
*crdno rt volume incr b.cond sa code area/factor ht str no.
11211601 122010000 0 1 1 339.560 1
11211602 122020000 0 1 1 391.285 2
11211603 122030000 0 1 1 178.821 3
11211604 122040000 0 1 1 178.821 4
11211605 118010000 0 1 1 212.368 5
*
*crdno s. type s. mult left heat right heat ht str no.
11211701 0 0.0 0.0 0.0 5
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
11211801 0.257 99.0 99.0 0.0 0.0 0.0 0.0 1.0 5
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
11211901 1.528 99.0 99.0 0.0 0.0 0.0 0.0 1.0 5
*
* heat structure 118:
* the following data represent the core baffle assembly *
*
*crdno heat str's mesh pts geometry init flag left coord
11161000 6 3 2 1 7.009
*
*crdno mesh locn flag mesh fwt flag
11161100 0 1
*

```

```

*
*crdno      no. intervals      rt coord
1118110:      2              7.144
*
*crdno      comp no.          interval no.
1118120:      1              2
*
*crdno      source value      mesh int. no.
1118130:      0.0              2
*
*crdno      temperature      mesh pt no.
1118140:      567.00           3
*
*crdno left volume  incr b.cond  sa code  area/factor  ht str no.
1118150:  118010000  10000  1  1  2.1110  6
*
*crdno rt volume  incr b.cond  sa code  area/factor  ht str no.
1118160:  118010000  10000  1  1  2.1110  6
*
*crdno s. type  s. mult  left heat  right heat  ht str no.
1118170:  0  0.0  0.0  0.0  6
*
*crdno equiv diam  heated len's  grid len's  grid cf's bf  ht str no.
1118180:  4.816  99.0  99.0  0.0  0.0  0.0  1.0  6
*
*crdno equiv diam  heated len's  grid len's  grid cf's bf  ht str no.
1118190:  1.432  99.0  99.0  0.0  0.0  0.0  0.0  1.0  6
*
* heat structure 118:
* the following data represent the upper core plate and fuel
* assembly top nozzles
*
*crdno heat str's  mesh pts  geometry  init flag  left coord
11181000  1  3  1  1  0.0
*
*crdno mesh lock flag  mesh fat flag
11181100  0  1
*
*crdno no. intervals      rt coord
1118110:      2              0.081
*
*crdno comp no.          interval no.
1118120:      1              2
*
*crdno source value      mesh int. no.
1118130:      0.0              2
*
*crdno temperature      mesh pt no.
1118140:      608.05           3
*
*crdno left volume  incr b.cond  sa code  area/factor  ht str no.
1118150:  118010000  0  1  1  144.005  1
*
*crdno rt volume  incr b.cond  sa code  area/factor  ht str no.
1118160:  118010000  0  1  1  144.005  1
*
*crdno s. type  s. mult  left heat  right heat  ht str no.
1118170:  0  0.0  0.0  0.0  1
*
*crdno equiv diam  heated len's  grid len's  grid cf's bf  ht str no.
1118180:  0.0  99.0  99.0  0.0  0.0  0.0  1.0  1

```

```

*
*crdno equiv diam  heated len's  grid len's  grid cf's bf  ht str no.
1118190:  0.0  99.0  99.0  0.0  0.0  0.0  1.0  1
*
* heat structure 115:
* the following data represent the core fuel pins
* in the average core
*
*crdno heat str's  mesh pts  geometry  init flag  left coord
11151000  2  3  1  1  0.0
*
*crdno mesh lock flag  mesh fat flag
11151100  0  1
*
*crdno no. intervals      rt coord
1115110:      2              0.154
*
*crdno comp no.          interval no.
1115120:      1              2
*
*crdno source value      mesh int. no.
1115130:      0.0              2
*
*crdno temperature      mesh pt no.
1115140:      549.51           3
*
*crdno left volume  incr b.cond  sa code  area/factor  ht str no.
1115150:  110100000  0  1  1  516.448  1
1115160:  110100000  0  1  1  213.223  2
*
*crdno rt volume  incr b.cond  sa code  area/factor  ht str no.
1115160:  110100000  0  1  1  516.448  1
1115162:  110100000  0  1  1  213.223  2
*
*crdno s. type  s. mult  left heat  right heat  ht str no.
1115170:  0  0.0  0.0  0.0  2
*
*crdno equiv diam  heated len's  grid len's  grid cf's bf  ht str no.
1115180:  0.0  99.0  99.0  0.0  0.0  0.0  1.0  1
1115182:  0.0  99.0  99.0  0.0  0.0  0.0  1.0  2
*
*crdno equiv diam  heated len's  grid len's  grid cf's bf  ht str no.
1115190:  0.0  99.0  99.0  0.0  0.0  0.0  1.0  1
1115192:  0.0  99.0  99.0  0.0  0.0  0.0  1.0  2
*
* heat structure 114:
* the following data represent the core fuel pins
* in the average core
*
*crdno heat str's  mesh pts  geometry  init flag  left coord
11141000  0  2  2  1  0.0
*
*crdno mesh lock flag  mesh fat flag
11141100  0  1
*
*crdno no. intervals      rt coord
1114110:      0              0.0148
1114112:      1              0.01517

```

```

1141183      2      0.01767
*
*crdno      comp no.      interval no.
1141201      1      5
1141202      2      6
1141203      3      8
*
*crdno      source value      mesh int. no.
1141301      0.9500      1
1141302      0.9600      2
1141303      1.0200      3
1141304      1.1500      4
1141305      1.3754      5
1141307      0.0      8
*
*crdno      temperature      mesh pt no.
1141401      1507.0      1
1141402      1291.0      2
1141403      711.0      6
1141404      636.0      7
1141406      605.0      8
*
*crdno      left volume      incr      b.cond      sa code      area/factor      ht str no.
1141501      0      0      0      0      0.0      1
1141502      0      0      0      0      0.0      2
1141503      0      0      0      0      0.0      3
1141504      0      0      0      0      0.0      4
1141505      0      0      0      0      0.0      5
1141506      0      0      0      0      0.0      6
*
*crdno      rl volume      incr      b.cond      sa code      area/factor      ht str no.
1141601      11401000      10000      1      0      7506.45      5
11416LJ      11406000      0      1      0      5126.24      6
*
*crdno      s. type      s mult      left heat      right heat      ht str no.
1141701      100      0.100      0.0      0.0      1
1141702      100      0.124      0.0      0.0      2
1141703      100      0.191      0.0      0.0      3
1141704      100      0.190      0.0      0.0      4
1141705      100      0.177      0.0      0.0      5
1141706      100      0.113      0.0      0.0      6
*
*crdno      equiv diam      heated len's      grid len's      grid cf's      bf ht str no.
1141901      0.04687      1.055 10.045      0.991 0.993      1.0 1.0 1.0 1
1141902      0.04687      2.166 8.834      0.993 0.993      1.0 1.1 1.0 2
1141903      0.04687      5.277 6.723      0.993 0.993      1.0 1.0 1.0 3
1141904      0.04687      7.388 4.612      0.993 0.993      1.0 1.0 1.0 4
1141905      0.04687      9.499 2.501      0.993 0.993      1.0 1.0 1.0 5
1141906      0.04687      11.277 0.723      0.993 0.993      1.0 1.0 1.0 6
*
$-----$
$loop a heat structures $
$-----$
* loops a,b,and c hot leg heat structures *
$-----$
*
*crdno      heat str's      mesh pts      geometry      init flag      left coord
1204100      12      3      2      -1      1.208
*
*crdno      mesh sock flag      mesh fat flag
1204110      0      1
*
*crdno      no. intervals      rl coord

```

```

12041101      2      1.417
*
*crdno      comp no.      interval no.
12041201      1      2
*
*crdno      source value      mesh int. no.
12041301      0.0      2
*
*crdno      temperature      mesh pt no.
12041401      607.71      3
*
*crdno      left volume      incr      b.cond      sa code      area/factor      ht str no.
12041501      204010000      0      1      1      5.3105      1
12041502      204020000      0      1      1      5.3105      2
12041503      204030000      0      1      1      5.3105      3
12041504      204040000      0      1      1      6.7932      4
12041505      204050000      0      1      1      5.3105      5
12041506      204060000      0      1      1      5.3105      6
12041507      204070000      0      1      1      5.3105      7
12041508      204080000      0      1      1      6.7932      8
12041509      204090000      0      1      1      5.3105      9
12041510      204100000      0      1      1      5.3105      10
12041511      204110000      0      1      1      5.3105      11
12041512      204120000      0      1      1      6.7932      12
*
*crdno      rl volume      incr      b.cond      sa code      area/factor      ht str no.
12041601      0      0      0      1      5.3105      1
12041602      0      0      0      1      5.3105      2
12041603      0      0      0      1      5.3105      3
12041604      0      0      0      1      6.7932      4
12041605      0      0      0      1      5.3105      5
12041606      0      0      0      1      5.3105      6
12041607      0      0      0      1      5.3105      7
12041608      0      0      0      1      6.7932      8
12041609      0      0      0      1      5.3105      9
12041610      0      0      0      1      5.3105      10
12041611      0      0      0      1      5.3105      11
12041612      0      0      0      1      6.7932      12
*
*crdno      s. type      s mult      left heat      right heat      ht str no.
12041701      0      0.0      0.0      0.0      12
*
*crdno      equiv diam      heated len's      grid len's      grid cf's      bf ht str no.
12041821      2.0      99.0 99.0      0.0 0.0      0.0 0.0 1.0 12
*
*crdno      curr flags      hyd diam      equiv diam      length      ht str no.
$-----$
$loop a steam generator inlet plenum $
$-----$
$      ht str no.      inlet plen
*
*htstr      ht str's      m-p's      geom      init i.coord      ref      k.vol      exl      incr
1206100      1      0      3      1      4.811      0
*
*htstr      mesh sock      mesh fat
1206110      0      1
*
*htstr      intervals      rl coord
12061101      1      3.836
12061102      4      5.633
*
*htstr      comp'n no.      interval
12061201      1

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12061202      2      0
*htstr      source      interval
12061301      0.0      5
*htstr      temp      mesh pt.
12061401      606.71      6
*htstr      left vol      incr      b.cond      sa code      area/factor      ht str no.
12061501      206010000      0      1      1      0.25      1
*htstr      right vol      incr      b.cond      sa code      area/factor      ht str no.
12061601      0      0      0      1      1      0.25      1
*htstr      s. type      s. mult      left heat      right heat      ht str no.
12061701      0      0      0      0      1
*crdno      equiv diam      heated len's      grid len's      grid cf's bf      ht str no.
12061801      0      99.0      99.0      0.0      0.0      0.0      0.0      1.0      1
*****
$eg tubes
$
-----
$      ht str no. 2081      eg tubes
-----
*htstr      ht str      n pts      geom      init      i.coord      refl      b.vol      axl. incr
12081000      8      6      2      1      0.0323      0
*htstr      mesh locn      mesh fat
12081100      0      1
*htstr      intervals      rt. coord
12081101      5      0.0365
*htstr      compon no.      interval
12081201      3      5
*htstr      source      interval
12081301      0.0      5
*htstr      temp      mesh pt.
12081401      557.71      6
*htstr      left vol      incr      b.cond      sa code      area/factor      ht str no.
12081501      206010000      0      1      1      19335.4      1
12081502      206020000      10000      1      1      25178.5      2
12081503      206030000      0      1      1      25178.5      3
12081504      206040000      0      1      1      25178.5      4
12081505      206040000      0      1      1      25178.5      5
12081506      206030000      0      1      1      25178.5      6
12081507      206020000      0      1      1      25178.5      7
12081508      206010000      0      1      1      19335.4      8
*htstr      s. type      s. mult      left heat      right heat      ht str no.
12081701      0      0      0      0      8
*crdno      equiv diam      heated len's      grid len's      grid cf's bf      ht str no.
12081801      0      99.0      99.0      0.0      0.0      2.0      0.0      1.0      8

```

```

*
*crdno      equiv diam      heated len's      grid len's      grid cf's bf      ht str no.
12081901      0.034      99.0      99.0      0.0      0.0      0.0      0.0      1.0      8
*****
$tube sheet
$
-----
$      ht str no. 2082      tube sheet
-----
*htstr      ht str      n pts      geom      init      i.coord      refl      b.vol      axl. incr
12082000      2      6      1      1      0.0      0
*htstr      mesh locn      mesh fat
12082100      0      1
*htstr      intervals      rt. coord
12082101      5      0.0537
*htstr      compon no.      interval
12082201      2      6
*htstr      source      interval
12082301      0.0      6
*htstr      temp      mesh pt.
12082401      598.02      6
*htstr      left vol      incr      b.cond      sa code      area/factor      ht str no.
12082501      208010000      0      1      0      1185.5      1
12082502      208080000      0      1      0      1185.5      2
*htstr      right vol      incr      b.cond      sa code      area/factor      ht str no.
12082601      0      0      0      0      0      1185.5      2
*htstr      s. type      s. mult      left heat      right heat      ht str no.
12082701      0      0      0      0      2
*crdno      equiv diam      heated len's      grid len's      grid cf's bf      ht str no.
12082801      0      99.0      99.0      0.0      0.0      0.0      0.0      1.0      2
*****
$outlet plenum
$
-----
$      ht str no. 2101      outlet pl
-----
*htstr      ht str      n pts      geom      init      i.coord      refl      b.vol      axl. incr
12101000      1      6      3      1      4.817      0
*htstr      mesh locn      mesh fat
12101100      2081      1
*htstr      temp      mesh pt.
12101401      547.7      6
*htstr      left vol      incr      b.cond      sa code      area/factor      ht str no.
12101501      210010000      0      1      1      0.25      1
*htstr      right vol      incr      b.cond      sa code      area/factor      ht str no.
12101601      0      0      0      1      1      0.25      1
*htstr      s. type      s. mult      left heat      right heat      ht str no.
12101701      0      0      0      0      1
*crdno      equiv diam      heated len's      grid len's      grid cf's bf      ht str no.

```



```

12121001 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*****
* loops a,b and c primary piping heat structures *
* between the s.g.s and rcd.s *
*****
*crdno heat str's mesh pts geometry init flag left coord
12121000 15 3 2 1 1.292
*
*crdno mesh locn flag mesh fat flag
12121100 0 1
*
*crdno no. intervals rt. coord
12121101 2 1.513
*
*crdno comp no. interval no.
12121201 1 2
*
*crdno source value mesh int. no.
12121301 0.0 2
*
*crdno temperature mesh pt no.
12121401 549.39 3
*
*crdno left volume incr b.cond sa code area/factor ht str no.
12121501 212010000 0 1 1 4.9599 1
12121502 212020000 0 1 1 2.7219 2
12121503 212030000 0 1 1 7.1209 3
12121504 212040000 0 1 1 4.2250 4
12121505 212050000 0 1 1 7.1209 5
12121506 312010000 0 1 1 4.9599 6
12121507 312020000 0 1 1 2.7219 7
12121508 312030000 0 1 1 7.1209 8
12121509 312040000 0 1 1 4.2250 9
12121510 312050000 0 1 1 7.1209 10
12121511 412010000 0 1 1 4.9599 11
12121512 412020000 0 1 1 2.7219 12
12121513 412030000 0 1 1 7.1209 13
12121514 412040000 0 1 1 4.2250 14
12121515 412050000 0 1 1 7.1209 15
*
*crdno rt volume incr b.cond sa code area/factor ht str no.
12121601 0 0 0 1 1 4.9599 1
12121602 0 0 0 1 1 2.7219 2
12121603 0 0 0 1 1 7.1209 3
12121604 0 0 0 1 1 4.2250 4
12121605 0 0 0 1 1 7.1209 5
12121606 0 0 0 1 1 4.9599 6
12121607 0 0 0 1 1 2.7219 7
12121608 0 0 0 1 1 7.1209 8
12121609 0 0 0 1 1 4.2250 9
12121610 0 0 0 1 1 7.1209 10
12121611 0 0 0 1 1 4.9599 11
12121612 0 0 0 1 1 2.7219 12
12121613 0 0 0 1 1 7.1209 13
12121614 0 0 0 1 1 4.2250 14
12121615 0 0 0 1 1 7.1209 15
*
*crdno s. type s. mult left heat right heat ht str no.
12121701 0 0.0 0.0 0.0 15
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.

```

```

12121801 0.0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 15
*
*crdno corr flags hyd diam equiv diam length ht str no.
*****
* loops a,b and c cold leg heat structures *
*****
*crdno heat str's mesh pts geometry init flag left coord
12121800 12 3 2 1 1.146
*
*crdno mesh locn flag mesh fat flag
12121100 0 1
*
*crdno no. intervals rt. coord
12121101 2 1.346
*
*crdno comp no. interval no.
12121201 1 2
*
*crdno source value mesh int. no.
12121301 0.0 2
*
*crdno temperature mesh pt no.
12121401 549.74 3
*
*crdno left volume incr b.cond sa code area/factor ht str no.
12121501 218010000 0 1 1 3.9233 1
12121502 218020000 0 1 1 5.4584 2
12121503 220010000 0 1 1 5.4584 3
12121504 220020000 0 1 1 5.4584 4
12121505 318010000 0 1 1 3.9233 5
12121506 318020000 0 1 1 5.4584 6
12121507 320010000 0 1 1 3.9233 7
12121508 320020000 0 1 1 5.4584 8
12121509 418010000 0 1 1 3.9233 9
12121510 418020000 0 1 1 5.4584 10
12121511 420010000 0 1 1 5.4584 11
12121512 420020000 0 1 1 5.4584 12
*
*crdno rt volume incr b.cond sa code area/factor ht str no.
12121601 0 0 0 1 1 3.9233 1
12121602 0 0 0 1 1 5.4584 2
12121603 0 0 0 1 1 5.4584 3
12121604 0 0 0 1 1 5.4584 4
12121605 0 0 0 1 1 3.9233 5
12121606 0 0 0 1 1 5.4584 6
12121607 0 0 0 1 1 5.4584 7
12121608 0 0 0 1 1 5.4584 8
12121609 0 0 0 1 1 3.9233 9
12121610 0 0 0 1 1 5.4584 10
12121611 0 0 0 1 1 5.4584 11
12121612 0 0 0 1 1 5.4584 12
*
*crdno s. type s. mult left heat right heat ht str no.
12121701 0 0.0 0.0 0.0 12

```

```

*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
12121801 0.0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 15
*****
* stream generator & secondary heat structures *
*****
$
$eq shell, above feeding
$

```

```

$-----*
          ht str no. 2541          shell,1
$-----*
*htstr ht str n pts geom init l.coord refl b.vol axl. incr
12541000 1 6 2 1 6.59 0
*
*htstr mesh locn mesh fat
12541100 0 1
*
*htstr intervals rt. coord
12541101 5 6.882
*
*htstr compn no. interval
12541201 2 5
*
*htstr source interval
12541301 0.0 5
*
*htstr temp mesh pt.
12541401 518.92 6
*
*htstr left vol incr b.cond sa code area/factor ht str no.
12541501 25401000 0 1 1 7.88 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
12541601 0 0 0 1 7.08 1
*
*htstr s. type s. mult left heat right heat ht str no.
12541701 0 0 0 0
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
12541801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$-----*
$g shell, below feeding
$-----*
$-----*
          ht str no. 2581          shell,2
$-----*
*htstr ht str n pts geom init l.coord refl b.vol axl. incr
12581000 1 6 2 1 6.59 0
*
*htstr mesh locn mesh fat
12581100 2541 1
*
*htstr temp fig
12581400 2541
*
*htstr left vol incr b.cond sa code area/factor ht str no.
12581501 25801000 0 1 1 4.405 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
12581601 0 0 0 1 4.405 1
*
*htstr s. type s. mult left heat right heat ht str no.
12581701 0 0 0 0
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
12581801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$-----*
$g shell, at transition cone
$-----*
$-----*
          ht str no. 2621          shell,3
$-----*

```

```

*htstr ht str n pts geom init l.coord refl b.vol axl. incr
12621000 1 6 2 1 5.648 0
*
*htstr mesh locn mesh fat
12621100 0 1
*
*htstr intervals rt. coord
12621101 5 5.925
*
*htstr compn no. interval
12621201 2 5
*
*htstr source interval
12621301 0.0 5
*
*htstr temp mesh pt.
12621401 505.80 6
*
*htstr left vol incr b.cond sa code area/factor ht str no.
12621501 26201000 0 1 1 7.834 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
12621601 0 0 0 1 7.834 1
*
*htstr s. type s. mult left heat right heat ht str no.
12621701 0 0 0 0
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
12621801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$-----*
$g shell, below transition cone
$-----*
$-----*
          ht str no. 2622          shell,4
$-----*
*htstr ht str n pts geom init l.coord refl b.vol axl. incr
12622000 3 6 2 1 5.08 0
*
*htstr mesh locn mesh fat
12622100 0 1
*
*htstr intervals rt. coord
12622101 5 5.298
*
*htstr compn no. interval
12622201 2 5
*
*htstr source interval
12622301 0.0 5
*
*htstr temp mesh pt.
12622402 505.59 8
*
*htstr left vol incr b.cond sa code area/factor ht str no.
12622501 26202000 10000 1 1 7.834 2
12622502 262040000 0 1 1 6.016 3
*
*htstr right vol incr b.cond sa code area/factor ht str no.
12622601 0 0 0 1 7.834 2
12622602 0 0 0 1 6.016 3
*
*htstr s. type s. mult left heat right heat ht str no.
12622701 0 0 0 0

```

```

*crdno  equiv diam  heated len's  grid len's  grid cf's bf ht str no.
1262201  0      99.0  99.0  0.0  0.0  0.0  0.0  1.0  3
$-----$
$wrapper, below transition cone
$-----$
$      ht str no. 2651      wrapper,1
$-----$
*htstr  ht str  # pts geom  init  l.coord  refl  b.vol  axl. incr
1262100  3      4      2      1      4.863  0
*
*htstr      mesh locn      mesh fat
1262100      0              1
*
*htstr      intervals      rt. coord
1262101      3              4.894
*
*htstr      compxn no.      interval
12621201     2              3
*
*htstr      source      interval
12621301     0.0          3
*
*htstr      temp      mesh pt.
12621401     502.41      4
*
*htstr  left vol  incr  b.cond  #4 code  area/factor  ht str no.
12621501 26010000  0      1      1      6.018  1
12621502 26020000 10000  1      1      7.834  3
*
*htstr  right vol  incr  b.cond  #4 code  area/factor  ht str no.
12621601 262040000  0      1      1      6.018  1
12621602 262030000 -10000  1      1      7.834  3
*
*htstr  s. type  s. mult  left heat  right heat  ht str no.
12621701  0      0      0      0      3
*
*crdno  equiv diam  heated len's  grid len's  grid cf's bf ht str no.
12621801  0.130  99.0  99.0  0.0  0.0  0.0  0.0  1.0  3
*
*crdno  equiv diam  heated len's  grid len's  grid cf's bf ht str no.
12621901  0.130  99.0  99.0  0.0  0.0  0.0  0.0  1.0  3
$-----$
$wrapper, at transition cone
$-----$
$      ht str no. 2662      wrapper,2
$-----$
*htstr  ht str  # pts geom  init  l.coord  refl  b.vol  axl. incr
1262200  1      4      2      1      4.902  0
*
*htstr      mesh locn      mesh fat
1262100      0              1
*
*htstr      intervals      rt. coord
1262101      3              4.937
*
*htstr      compxn no.      interval
1262201     2              3
*
*htstr      source      interval
1262301     0.0          3
*

```

```

*htstr      temp      mesh pt.
1262401     511.13      4
*
*htstr  left vol  incr  b.cond  #4 code  area/factor  ht str no.
1262501 26040000  0      1      1      7.834  1
*
*htstr  right vol  incr  b.cond  #4 code  area/factor  ht str no.
1262601 262010000  0      1      1      7.834  1
*
*htstr  s. type  s. mult  left heat  right heat  ht str no.
1262701  0      0      0      0      1
*
*crdno  equiv diam  heated len's  grid len's  grid cf's bf ht str no.
1262801  0.130  99.0  99.0  0.0  0.0  0.0  0.0  1.0  1
*
*crdno  equiv diam  heated len's  grid len's  grid cf's bf ht str no.
1262901  0.130  99.0  99.0  0.0  0.0  0.0  0.0  1.0  1
$-----$
$wrapper, above transition cone
$-----$
$      ht str no. 2701      wrapper,3
$-----$
*htstr  ht str  # pts geom  init  l.coord  refl  b.vol  axl. incr
1270100  1      4      2      1      5.264  0
*
*htstr      mesh locn      mesh fat
1270100      0              1
*
*htstr      intervals      rt. coord
1270101      3              5.295
*
*htstr      compxn no.      interval
12701201     2              3
*
*htstr      source      interval
12701301     0.0          3
*
*htstr      temp      mesh pt.
12701401     512.60      4
*
*htstr  left vol  incr  b.cond  #4 code  area/factor  ht str no.
12701501 27010000  0      1      1      4.405  1
*
*htstr  right vol  incr  b.cond  #4 code  area/factor  ht str no.
12701601 256010000  0      1      1      4.405  1
*
*htstr  s. type  s. mult  left heat  right heat  ht str no.
12701701  0      0      0      0      1
*
*crdno  equiv diam  heated len's  grid len's  grid cf's bf ht str no.
12701801  0      99.0  99.0  0.0  0.0  0.0  0.0  1.0  1
*
*crdno  equiv diam  heated len's  grid len's  grid cf's bf ht str no.
12701901  0      99.0  99.0  0.0  0.0  0.0  0.0  1.0  1
$-----$
$wrapper, around primary (swirl vane) separator
$-----$
$      ht str no. 2741      wrapper,4
$-----$
*htstr  ht str  # pts geom  init  l.coord  refl  b.vol  axl. incr
1274100  1      4      2      1      5.588  0
*

```

```

*htstr 12741100 mesh locn mesh fat
* 0 1
*
*htstr 12741101 intervals rl coord
* 3 5.6200
*
*htstr 12741201 compvn no. interval
* 2 3
*
*htstr 12741301 source interval
* 0.0 3
*
*htstr 12741401 temp mesh pt.
* 517.96 4
*
*htstr 12741501 left vol incr b.cond sa code area/factor ht str no.
* 274010000 0 1 1 7.88 1
*
*htstr 12741601 right vol incr b.cond sa code area/factor ht str no.
* 254010000 0 1 1 7.88 1
*
*htstr 12741701 s. type s. mult left heat right heat ht str no.
* 0 0 0 0 1
*
*crdno 12741801 equiv diam heated len's grid len's grid cf's bf ht str no.
* 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
*crdno 12741901 equiv diam heated len's grid len's grid cf's bf ht str no.
* 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$.....$
$primary separator (swirl vane) $
$ ht str no. 2742 swirl vane $
*
*htstr 12742000 ht str's m pts geom init l.coord refl b.vol axl. incr
* 1 4 1 1 0.0 0
*
*htstr 12742100 mesh locn mesh fat
* 0 1
*
*htstr 12742101 intervals rl coord
* 3 0.03125
*
*htstr 12742201 compvn no. interval
* 2 3
*
*htstr 12742301 source interval
* 0.0 3
*
*htstr 12742401 temp mesh pt.
* 517.96 4
*
*htstr 12742501 left vol incr b.cond sa code area/factor ht str no.
* 274010000 0 1 1 647.9 1
*
*htstr 12742601 right vol incr b.cond sa code area/factor ht str no.
* 274010000 0 1 1 647.9 1
*
*htstr 12742701 s. type s. mult left heat right heat ht str no.
* 0 0 0 0 1
*
*crdno 12742801 equiv diam heated len's grid len's grid cf's bf ht str no.

```

```

12742801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
*crdno 12742901 equiv diam heated len's grid len's grid cf's bf ht str no.
* 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$.....$
$secondary separator (dryer vane) $
$ ht str no. 2781 shell,5 $
*
*htstr 12781000 ht str's m pts geom init l.coord refl b.vol axl. incr
* 1 6 2 1 6.59 0
*
*htstr 12781100 mesh locn mesh fat
* 2541 1
*
*htstr 12781400 temp fig
* 2541
*
*htstr 12781501 left vol incr b.cond sa code area/factor ht str no.
* 278010000 0 1 1 5.29 1
*
*htstr 12781601 right vol incr b.cond sa code area/factor ht str no.
* 0 0 0 1 5.29 1
*
*htstr 12781701 s. type s. mult left heat right heat ht str no.
* 0 0 0 0 1
*
*crdno 12781801 equiv diam heated len's grid len's grid cf's bf ht str no.
* 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$.....$
$secondary separator (dryer vane) $
$ ht str no. 2782 dryer $
*
*htstr 12782000 ht str's m pts geom init l.coord refl b.vol axl. incr
* 1 4 1 1 0.0 0
*
*htstr 12782100 mesh locn mesh fat
* 0 1
*
*htstr 12782101 intervals rl coord
* 3 0.02083
*
*htstr 12782201 compvn no. interval
* 2 3
*
*htstr 12782301 source interval
* 0.0 3
*
*htstr 12782401 temp mesh pt.
* 517.83 4
*
*htstr 12782501 left vol incr b.cond sa code area/factor ht str no.
* 278010000 0 1 1 2347. 1
*
*htstr 12782601 right vol incr b.cond sa code area/factor ht str no.
* 278010000 0 1 1 2347. 1
*
*htstr 12782701 s. type s. mult left heat right heat ht str no.
* 0 0 0 0 1
*
*crdno 12782801 equiv diam heated len's grid len's grid cf's bf ht str no.

```

```

1272201 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
*crdno equiv diam heated len's grid len's grid ct's bf ht str no.
1272201 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$-----$
$sg shell, at elevation of dryer, including ellipsoidal top cap $
$-----$
$ ht str no. 2821 shell 6 $
*
*htstr ht str n pts geom init l.coord refl b.vol axl incr
1282100 1 5 2 1 6.58 0
*
*htstr mesh loch mesh fat
1282100 0 1
*
*htstr intervals rt coord
1282101 5 6.0817
*
*htstr compn no. interval
1282101 2 5
*
*htstr source interval
12821301 0.0 5
*
*htstr temp mesh pt.
12821401 518.90 6
*
*htstr left vol incr b.cond sa code area/factor ht str no.
12821501 282010000 0 1 1 7.781 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
12821601 0 0 0 1 1 7.781 1
*
*htstr s. type s. mult left heat right heat ht str no.
12821701 0 0 0 0
*
*crdno equiv diam heated len's grid len's grid ct's bf ht str no.
12821801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$-----$
$loop b steam generator inlet plenum, u-tubes, outlet plenum h.s. $
$-----$
$inlet plenum $
$-----$
$ ht str no. 3061 inlet plen $
*
*htstr ht str n pts geom init l.coord refl b.vol axl incr
1306100 1 5 3 1 4.817 0
*
*htstr mesh loch mesh fat
1306100 0 1
*
*htstr intervals rt coord
1306101 1 4.838
1306102 4 5.623
*
*htstr compn no. interval
13061201 1 1
13061202 2 5
*
*htstr source interval
13061301 0.0 5

```

```

*
*htstr temp mesh pt.
13061401 606.11 6
*
*htstr left vol incr b.cond sa code area/factor ht str no.
13061501 306010000 0 1 1 0.25 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
13061601 0 0 0 1 1 0.25 1
*
*htstr s. type s. mult left heat right heat ht str no.
13061701 0 0 0 0
*
*crdno equiv diam heated len's grid len's grid ct's bf ht str no.
13061801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$-----$
$sg tubes $
$-----$
$ ht str no. 3081 sg tubes $
*
*htstr ht str n pts geom init l.coord refl b.vol axl incr
1308100 6 2 2 1 0.0323 0
*
*htstr mesh loch mesh fat
1308100 0 1
*
*htstr intervals rt coord
1308101 5 0.0365
*
*htstr compn no. interval
13081201 3 5
*
*htstr source interval
13081301 0.0 5
*
*htstr temp mesh pt.
13081401 550. 6
*
*htstr left vol incr b.cond sa code area/factor ht str no.
13081501 308010000 0 1 1 19235.4 1
13081502 308020000 10000 1 1 25178.5 7
13081503 308030000 0 1 1 19235.4 8
*
*htstr right vol incr b.cond sa code area/factor ht str no.
13081601 308010000 0 1 1 19235.4 1
13081602 308020000 0 1 1 25178.5 2
13081603 308030000 0 1 1 25178.5 3
13081604 308040000 0 1 1 25178.5 4
13081605 308040000 0 1 1 25178.5 5
13081606 308030000 0 1 1 25178.5 6
13081607 308020000 0 1 1 25178.5 7
13081608 308010000 0 1 1 19235.4 8
*
*htstr s. type s. mult left heat right heat ht str no.
13081701 0 0 0 0
*
*crdno equiv diam heated len's grid len's grid ct's bf ht str no.
13081801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 0
*
*crdno equiv diam heated len's grid len's grid ct's bf ht str no.
13081901 0.034 99.0 99.0 0.0 0.0 0.0 0.0 1.0 8
*
$-----$

```



```

* tube sheet
*
* ht str no. 3082 tube sheet
*
* ht str ht str mesh pts geom init l.coord refl b.vol axl incr
13082000 2 8 1 1 0.0 0
*
* ht str mesh locn mesh fat
13082100 0 1
*
* ht str intervals rt coord
13082101 5 0.0537
*
* ht str compn no. interval
13082201 2 5
*
* ht str source interval
13082301 0.0 5
*
* ht str temp mesh pt.
13082401 575.0 6
*
* ht str left vol incr b.cond sa code area/factor ht str no.
13082501 308010000 0 1 0 1185.5 1
13082502 308080000 0 1 0 1185.5 2
*
* ht str right vol incr b.cond sa code area/factor ht str no.
13082601 0 0 0 1 1185.5 2
*
* ht str s. type s. mult left heat right heat ht str no.
13082701 0 0 0 0
*
* crdno equiv diam heated len's grid len's grid cf's bf ht str no.
13082801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 2
*
*****
* outlet plenum
*
* ht str no. 3101 outlet pl
*
* ht str ht str mesh pts geom init l.coord refl b.vol axl incr
13101000 1 8 3 1 4.817 0
*
* ht str mesh locn mesh fat
13101100 3051 1
*
* ht str temp mesh pt.
13101401 547.6 6
*
* ht str left vol incr b.cond sa code area/factor ht str no.
13101501 310010000 0 1 1 0.25 1
*
* ht str right vol incr b.cond sa code area/factor ht str no.
13101601 0 0 0 1 0.25 1
*
* ht str s. type s. mult left heat right heat ht str no.
13101701 0 0 0 0
*
* crdno equiv diam heated len's grid len's grid cf's bf ht str no.
13101801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
*****
* pressurizer wall heat structures
*

```

```

*****
*
* crdno heat str's mesh pts geometry init flag left coord
13401000 8 6 2 1 3.500
*
* crdno mesh locn flag mesh fat flag
13401100 0 1
*
* crdno no. intervals rt coord
13401101 2 3.616
13401102 3 3.842
*
* crdno comp no. interval no.
13401201 1 2
13401202 2 5
*
* crdno source value mesh int. no.
13401301 0.0 5
*
* crdno temperature mesh pt no.
13401401 652.70 6
*
* crdno left volume incr b.cond sa code area/factor ht str no.
13401501 340010000 0 1 1 3.5000 1
13401502 341010000 0 1 1 4.8522 2
13401503 341020000 0 1 1 4.8522 3
13401504 341030000 0 1 1 4.8522 4
13401505 341040000 0 1 1 4.8522 5
13401506 341050000 0 1 1 4.8522 6
13401507 341060000 0 1 1 4.8522 7
13401508 341070000 0 1 1 3.5000 8
*
* crdno rt volume incr b.cond sa code area/factor ht str no.
13401601 0 0 0 1 3.5000 1
13401602 0 0 0 1 4.8522 2
13401603 0 0 0 1 4.8522 3
13401604 0 0 0 1 4.8522 4
13401605 0 0 0 1 4.8522 5
13401606 0 0 0 1 4.8522 6
13401607 0 0 0 1 4.8522 7
13401608 0 0 0 1 3.5000 8
*
* crdno s. type s. mult left heat right heat ht str no.
13401701 0 0 0 0 0
*
* crdno equiv diam heated len's grid len's grid cf's bf ht str no.
13401801 0.0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 8
*
*****

```

```

* pressurizer surge line heat structures
*
*****
*
* crdno heat str's mesh pts geometry init flag left coord
13431000 3 3 2 1 0.498
*
* crdno mesh locn flag mesh fat flag
13431100 0 1
*
* crdno no. intervals rt coord
13431101 2 0.531
*
* crdno comp no. interval no.
13431201 1 2
*

```

```

*crdno      source value      mesh int. no.
13431301      0.0                      2
*
*crdno      temperature      mesh pt no.
13431401      647.98                    3
*
*crdno left volume  incr b cond  sa code  area/factor  ht str no.
13431501  343010000    0 1 1 1 12.5549 1
13431502  343200000    0 1 1 1 22.3757 2
13431503  343300000    0 1 1 1 22.3757 3
*
*crdno rt volume    incr b cond  sa code  area/factor  ht str no.
13431601  0 0 0 1 1 12.5549 1
13431602  0 0 0 1 1 22.3757 2
13431603  0 0 0 1 1 22.3757 3
*
*crdno s. type  s. mult  left heat  right heat  ht str no.
13431701  0 0.0 0.0 0.0 3
*
*crdno equiv diam  heated len's  grid len's  grid cf's bf ht str no.
13431801  0.0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 3
*
*.....*
* pressurizer proportional heaters heat structures *
*.....*
*
*crdno heat str's  mesh pts  geometry  init flag  left coord
13411000  1 5 2 1 0.0
*
*crdno      mesh locn flag      mesh int flag
13411100      0 1
*
*crdno      no. intervals      rt. coord
13411101      2 0.0627
13411102      2 0.0727
*
*crdno      comp no.      interval no.
13411201      1 2
13411202      1 4
*
*crdno      source value      mesh int. no.
13411301      1.0 2
13411302      0.0 4
*
*crdno      temperature      mesh pt no.
13411401      649.98 5
*
*crdno left volume  incr b cond  sa code  area/factor  ht str no.
13411501  0 0 0 1 1 71.520
*
*crdno rt volume    incr b cond  sa code  area/factor  ht str no.
13411601  341070000    0 1 1 1 71.520
*
*crdno s. type  s. mult  left heat  right heat  ht str no.
13411701  10216 1.0 0.0 0.0 1
*
*crdno equiv diam  heated len's  grid len's  grid cf's bf ht str no.
13411801  0.0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
*.....*
* pressurizer backup heaters heat structures *
*.....*

```

```

*crdno heat str's  mesh pts  geometry  init flag  left coord
13421000  1 5 2 1 0.0
*
*crdno      mesh locn flag      mesh int flag
13421100      0 1
*
*crdno      no. intervals      rt. coord
13421101      2 0.0627
13421102      2 0.0727
*
*crdno      comp no.      interval no.
13421201      1 2
13421202      1 4
*
*crdno      source value      mesh int. no.
13421301      1.0 2
13421302      0.0 4
*
*crdno      temperature      mesh pt no.
13421401      649.98 5
*
*crdno left volume  incr b cond  sa code  area/factor  ht str no.
13421501  0 0 0 1 1 160.92
*
*crdno rt volume    incr b cond  sa code  area/factor  ht str no.
13421601  341070000    0 1 1 1 160.92
*
*crdno s. type  s. mult  left heat  right heat  ht str no.
13421701  10217 1.0 0.0 0.0 1
*
*crdno equiv diam  heated len's  grid len's  grid cf's bf ht str no.
13421801  0.0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$loop b steam generator secondary heat structures $
$.....$
$ ht str no. 254: shell,1 $
$.....$
*htstr ht str's  mesh pts  geom  init l.coord  refl b.vol  axl. incr
13541000  1 6 2 1 6.59 0
*
*htstr      mesh locn      mesh int
13541100      0 1
*
*htstr      intervals      rt coord
13541101      5 0.862
*
*htstr      compn no.      interval
13541201      2 5
*
*htstr      source      interval
13541301      0.0 5
*
*htstr      temp      mesh pt.
13541401      519.61 6
*
*htstr left vol  incr b cond  sa code  area/factor  ht str no.
13541501  354010000    0 1 1 1 7.88
*
*htstr right vol  incr b cond  sa code  area/factor  ht str no.
13541601  0 0 0 1 1 7.88
*
*htstr s. type  s. mult  left heat  right heat  ht str no.
13541701  0 0 0 0 1

```

```

*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
13541801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$*****
$eg shell, below feeding
$-----
$ ht str no. 3581 shell.2
$-----
*htstr ht str's n pts geom init l.coord refl b.vol axl incr
13581000 1 6 2 1 6.59 0
*
*htstr mesh loch mesh fat
13581100 3541 1
*
*htstr temp fig
13581400 3541
*
*htstr left vol incr b.cond sa code area/factor ht str no.
13581501 358010000 0 1 1 4.405 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
13581601 0 0 0 1 4.405 1
*
*htstr s. type s. mult left heat right heat ht str no.
13581701 0 0 0 0
*

```

```

*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
13621801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$*****
$eg shell, at transition cone
$-----
$ ht str no. 3621 shell.3
$-----
*htstr ht str's n pts geom init l.coord refl b.vol axl incr
13621000 1 6 2 1 5.64P 0
*
*htstr mesh loch mesh fat
13621100 0 1
*
*htstr intervals rt. coord
13621101 5 5.925
*
*htstr compxn no. interval
13621201 2 5
*
*htstr source interval
13621301 0.0 5
*
*htstr temp mesh pt.
13621401 505.27 6
*
*htstr left vol incr b.cond sa code area/factor ht str no.
13621501 362010000 0 1 1 7.834 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
13621601 0 0 0 1 7.834 1
*
*htstr s. type s. mult left heat right heat ht str no.
13621701 0 0 0 0
*

```

```

*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
13621801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$*****
$eg shell, below transition cone
$-----
$ ht str no. 3622 shell.4
$-----
*htstr ht str's n pts geom init l.coord refl b.vol axl incr
13622000 3 6 2 1 5.08 0
*
*htstr mesh loch mesh fat
13622100 0 1
*
*htstr intervals rt. coord
13622101 5 5.298
*
*htstr compxn no. interval
13622201 2 5
*
*htstr source interval
13622301 0.0 5
*
*htstr temp mesh pt.
13622402 505.47 6
*
*htstr left vol incr b.cond sa code area/factor ht str no.
13622501 362020000 10000 1 1 7.834 2
13622502 362940000 0 1 1 6.016 3
*
*htstr right vol incr b.cond sa code area/factor ht str no.
13622601 0 0 0 1 7.834 2
13622602 0 0 0 1 6.016 3
*
*htstr s. type s. mult left heat right heat ht str no.
13622701 0 0 0 0
*

```

```

*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
13661801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 3
*
$*****
$eg wrapper, below transition cone
$-----
$ ht str no. 3661 wrapper.1
$-----
*htstr ht str's n pts geom init l.coord refl b.vol axl incr
13661000 3 4 2 1 4.863 0
*
*htstr mesh loch mesh fat
13661100 0 1
*
*htstr intervals rt. coord
13661101 3 4.864
*
*htstr compxn no. interval
13661201 2 3
*
*htstr source interval
13661301 0.0 3
*
*htstr temp mesh pt.
13661401 500.19 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
13661501 366010000 0 1 1 6.016 1
*

```

```

*
* 13661502 36602000 10000 1 1 7.834 3
*
*htstr right vol incr b.cond sa code area/factor ht str no.
13661601 362040000 0 1 1 6.016 1
13661602 362030000 -10000 1 1 7.834 3
*
*htstr s. type s. mult left heat right heat ht str no.
13661701 0 0 0 0
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
13661801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 3
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
13661901 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 3
*
$-----$
$ wrapper, at transition cone $
$ ht str no. 3662 wrapper,2 $
$-----$
*htstr ht str's n pts geom init l.coord refl b.vol axl. incr
13662000 1 4 2 1 4.952 0
*
*htstr mesh loch mesh fat
13662100 0 1
*
*htstr intervals rt. coord
13662101 3 4.9337
*
*htstr compxn no. interval
13662201 2 3
*
*htstr source interval
13662301 0.0 3
*
*htstr temp mesh pt.
13662401 510.81 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
13662501 366040000 0 1 1 7.834 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
13662601 362010000 0 1 1 7.834 1
*
*htstr s. type s. mult left heat right heat ht str no.
13662701 0 0 0 0
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
13662801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
13662901 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$-----$
$ wrapper, above transition cone $
$ ht str no. 3701 wrapper,3 $
$-----$
*htstr ht str's n pts geom init l.coord refl b.vol axl. incr
13701000 1 4 2 1 5.264 0
*
*htstr mesh loch mesh fat
13701100 0 1

```

```

*
*htstr intervals rt. coord
13701101 3 5.295
*
*htstr compxn no. interval
13701201 2 3
*
*htstr source interval
13701301 0.0 3
*
*htstr temp mesh pt.
13701401 512.28 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
13701501 370010000 0 1 1 4.405 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
13701601 358010000 0 1 1 4.405 1
*
*htstr s. type s. mult left heat right heat ht str no.
13701701 0 0 0 0
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
13701801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
13701901 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$-----$
$ wrapper, around primary (swirl vane) separator $
$ ht str no. 2741 wrapper,4 $
$-----$
*htstr ht str's n pts geom init l.coord refl b.vol axl. incr
13741000 1 4 2 1 5.5888 0
*
*htstr mesh loch mesh fat
13741100 0 1
*
*htstr intervals rt. coord
13741101 3 5.6250
*
*htstr compxn no. interval
13741201 2 3
*
*htstr source interval
13741301 0.0 3
*
*htstr temp mesh pt.
13741401 517.63 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
13741501 374010000 0 1 1 7.88 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
13741601 354010000 0 1 1 7.88 1
*
*htstr s. type s. mult left heat right heat ht str no.
13741701 0 0 0 0
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
13741801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.

```

```

13741901 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
$-----$
$primary separator (swirl vane) $
$-----$
$ ht str no. 3742 swirl vane
$-----$
*htstr ht str m pts geom init l.coord refl b.vol axl. incr
13742000 1 4 1 1 0.0 0
*
*htstr mesh locn mesh fat
13742100 0 1
*
*htstr intervals rt. coord
13742101 3 0.63125
*
*htstr compn no. interval
13742201 2 3
*
*htstr source interval
13742301 0.0 3
*
*htstr temp mesh pt.
13742401 517.63 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
13742501 374010000 0 1 0 847.7 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
13742601 374010000 0 1 0 847.7 1
*
*htstr s. type s. mult left heat right heat ht str no.
13742701 0 0 0 0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
13742801 0 19.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
13742901 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
$-----$
$seg shell, elevation of dryer $
$-----$
$ ht str no. 3781 shell, $
$-----$
*htstr ht str m pts geom init l.coord refl b.vol axl. incr
13781000 1 6 2 1 5.59 0
*
*htstr mesh locn mesh fat
13781100 3541 1
*
*htstr temp fig
13781400 3541
*
*htstr left vol incr b.cond sa code area/factor ht str no.
13781501 378010000 0 1 1 5.29 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
13781601 0 0 0 1 5.29 1
*
*htstr s. type s. mult left heat right heat ht str no.
13781701 0 0 0 0 1
*

```

```

*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
13781901 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
$-----$
$secondary separator (dryer vane) $
$-----$
$ ht str no. 3782 dryer
$-----$
*htstr ht str m pts geom init l.coord refl b.vol axl. incr
13782000 1 4 1 1 0.0 0
*
*htstr mesh locn mesh fat
13782100 0 1
*
*htstr intervals rt. coord
13782101 3 0.02083
*
*htstr compn no. interval
13782201 2 3
*
*htstr source interval
13782301 0.0 3
*
*htstr temp mesh pt.
13782401 517.51 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
13782501 378010000 0 1 0 2347. 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
13782601 378010000 0 1 0 2347. 1
*
*htstr s. type s. mult left heat right heat ht str no.
13782701 0 0 0 0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
13782901 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
13782901 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
$-----$
$seg shell, at elevation of dryer, including ellipsoidal top cap $
$-----$
$ ht str no. 3821 shell, $
$-----$
*htstr ht str m pts geom init l.coord refl b.vol axl. incr
13821000 1 6 2 1 4.59 0
*
*htstr mesh locn mesh fat
13821100 0 1
*
*htstr intervals rt. coord
13821101 5 6.8817
*
*htstr compn no. interval
13821201 2 5
*
*htstr source interval
13821301 0.0 5
*
*htstr temp mesh pt.
13821401 519.68 6
*

```



```

*htstr left vol incr b.cond sa code area/factor ht str no.
13821501 382010000 0 1 1 7.761 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
13821601 0 0 0 1 7.761 1
*
*htstr s. type s. mult left heat right heat ht str no.
13821701 0 0 0 0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
13821801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$-----$
$steam generator c heat structures $
$-----$
$inlet plenum $
$-----$
$ ht str no. 4061 inlet plen $
$-----$
*htstr ht str's w pts geom init l.coord refl b.vol axl. incr
14061000 1 6 3 1 4.617 0
*
*htstr mesh loch mesh fat
14061100 0 1
*
*htstr intervals ri. coord
14061101 1 4.838
14061102 4 5.633
*
*htstr compxn no. interval
14061201 1 1
14061202 2 5
*
*htstr source interval
14061301 0.0 5
*
*htstr temp mesh pt.
14061401 606.12 6
*
*htstr left vol incr b.cond sa code area/factor ht str no.
14061501 400010000 0 1 1 0.25 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
14061601 0 0 0 1 0.25 1
*
*htstr s. type s. mult left heat right heat ht str no.
14061701 0 0 0 0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
14061801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$-----$
$sg tubes $
$-----$
$ ht str no. 4081 sg tubes $
$-----$
*htstr ht str's w pts geom init l.coord refl b.vol axl. incr
14081000 8 6 2 1 0.0323 0
*
*htstr mesh loch mesh fat
14081100 0 1
*
*htstr intervals ri. coord

```

```

14081101 5 0.0365
*
*htstr compxn no. interval
14081201 3 5
*
*htstr source interval
14081301 0.0 5
*
*htstr temp mesh pt.
14081401 550.0 6
*
*htstr left vol incr b.cond sa code area/factor ht str no.
14081501 408010000 0 1 1 19325.4 1
14081502 408020000 10000 1 1 25178.5 7
14081503 408030000 0 1 1 19325.4 8
*
*htstr right vol incr b.cond sa code area/factor ht str no.
14081601 466010000 0 1 1 19325.4 1
14081602 466020000 0 1 1 25178.5 2
14081603 466030000 0 1 1 25178.5 3
14081604 466040000 0 1 1 25178.5 4
14081605 466040000 0 1 1 25178.5 5
14081606 466030000 0 1 1 25178.5 6
14081607 466020000 0 1 1 25178.5 7
14081608 466010000 0 1 1 19325.4 8
*
*htstr s. type s. mult left heat right heat ht str no.
14081701 0 0 0 0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
14081801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 8
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
14081901 0.034 99.0 99.0 0.0 0.0 0.0 0.0 1.0 8
*
$-----$
$tube sheet $
$-----$
$ ht str no. 4082 tube sheet $
$-----$
*htstr ht str's w pts geom init l.coord refl b.vol axl. incr
14082000 2 6 1 1 0.0 0
*
*htstr mesh loch mesh fat
14082100 0 1
*
*htstr intervals ri. coord
14082101 5 0.0537
*
*htstr compxn no. interval
14082201 2 5
*
*htstr source interval
14082301 0.0 5
*
*htstr temp mesh pt.
14082401 535.0 6
*
*htstr left vol incr b.cond sa code area/factor ht str no.
14082501 408010000 0 1 0 1185.5 1
14082502 408060000 0 1 0 1185.5 2
*
*htstr right vol incr b.cond sa code area/factor ht str no.
14082601 0 0 0 1 1185.5 2

```

```

*htstr s. type s. mult left heat right heat ht str no.
14082701 0 0 0 0 0 2
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
14082801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 2
*
$*****$
$ outlet plenum $
$
$ ht str no. 4101 outlet pl $
$
*htstr ht str's w pts geom init l.coord refl b.vol axl incr
14101000 1 6 3 1 4.817 0
*
*htstr mesh locn mesh fat
14101100 4061 1
*
*htstr temp mesh pt.
14101401 547.08 6
*
*htstr left vol incr b.cond sa code area/factor ht str no.
14101601 410010000 0 1 1 0.25 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
14101601 0 0 0 1 0.25 1
*
*htstr s. type s. mult left heat right heat ht str no.
14101701 0 0 0 0 0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
14101801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$*****$
$ sg shell, above feeding $
$
$ ht str no. 4541 shell,1 $
$
*htstr ht str's w pts geom init l.coord refl b.vol axl incr
14541000 1 6 2 1 1.59 0
*
*htstr mesh locn mesh fat
14541100 0 1
*
*htstr intervals rt coord
14541101 5 8.982
*
*htstr compon no. interval
14541201 2 5
*
*htstr source interval
14541301 0.0 5
*
*htstr temp mesh pt.
14541401 518.85 6
*
*htstr left vol incr b.cond sa code area/factor ht str no.
14541601 454010000 0 1 1 7.83 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
14541601 0 0 0 1 7.83 1
*
*htstr s. type s. mult left heat right heat ht str no.

```

```

14541701 0 0 0 0 0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
14541801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$*****$
$ sg shell, below feeding $
$
$ ht str no. 4641 shell,2 $
$
*htstr ht str's w pts geom init l.coord refl b.vol axl incr
14581000 1 6 2 1 6.59 0
*
*htstr mesh locn mesh fat
14581100 4541 1
*
*htstr temp fig
14581400 4541
*
*htstr left vol incr b.cond sa code area/factor ht str no.
14581501 458010000 0 1 1 4.405 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
14581601 0 0 0 1 4.405 1
*
*htstr s. type s. mult left heat right heat ht str no.
14581701 0 0 0 0 0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
14581801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$*****$
$ sg shell, at transition cone $
$
$ ht str no. 4821 shell,3 $
$
*htstr ht str's w pts geom init l.coord refl b.vol axl incr
14621000 1 6 2 1 5.648 0
*
*htstr mesh locn mesh fat
14621100 0 1
*
*htstr intervals rt coord
14621101 5 5.505
*
*htstr compon no. interval
14621201 2 5
*
*htstr source interval
14621301 0.0 5
*
*htstr temp mesh pt.
14621401 505.53 6
*
*htstr left vol incr b.cond sa code area/factor ht str no.
14621501 462010000 0 1 1 7.834 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
14621601 0 0 0 1 7.834 1
*
*htstr s. type s. mult left heat right heat ht str no.
14621701 0 0 0 0 0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.

```

```

14621001 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*****
$ wrapper, below transition cone
$
$ ht str no. 4622 shell,4
*****
*htstr ht str n pts geom init l.coord refl b.vol axl incr
14622000 3 6 2 1 5.08 0
*
*htstr mesh loch mesh fat
14622100 0 1
*
*htstr intervals rt.coord
14622101 5 5.296
*
*htstr compn no. interval
14622201 2 5
*
*htstr source interval
14622301 0.0 5
*
*htstr temp mesh pt.
14622402 505.52 6
*
*htstr left vol incr b.cond sa code area/factor ht str no.
14622501 46204000 10000 1 1 7.834 2
14622502 46204000 0 1 1 6.016 3
*
*htstr right vol incr b.cond sa code area/factor ht str no.
14622601 0 0 0 1 1 7.834 2
14622602 0 0 0 1 1 6.016 3
*
*htstr s. type s. mult left heat right heat ht str no.
14622701 0 0 0 0
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
14622801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 3
*****
$ wrapper, below transition cone
$
$ ht str no. 4661 wrapper,1
*****
*htstr ht str n pts geom init l.coord refl b.vol axl incr
14661000 3 4 2 1 4.863 0
*
*htstr mesh loch mesh fat
14661100 0 1
*
*htstr intervals rt.coord
14661101 3 4.894
*
*htstr compn no. interval
14661201 2 3
*
*htstr source interval
14661301 0.0 3
*
*htstr temp mesh pt.
14661401 509.44 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.

```

```

14661501 46601000 0 1 1 6.016 1
14661502 46602000 10000 1 1 7.834 3
*
*htstr right vol incr b.cond sa code area/factor ht str no.
14661601 46704000 0 1 1 6.016 1
14661602 46703000 -10000 1 1 7.834 3
*
*htstr s. type s. mult left heat right heat ht str no.
14661701 0 0 0 0
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
14661801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 2
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
14661901 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 3
*****
$ wrapper, above transition cone
$
$ ht str no. 4662 wrapper,2
*****
*htstr ht str n pts geom init l.coord refl b.vol axl incr
14662000 1 4 2 1 4.902 0
*
*htstr mesh loch mesh fat
14662100 0 1
*
*htstr intervals rt.coord
14662101 3 4.932
*
*htstr compn no. interval
14662201 2 3
*
*htstr source interval
14662301 0.0 3
*
*htstr temp mesh pt.
14662401 511.06 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
14662501 46604000 0 1 1 7.834 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
14662601 46201000 0 1 1 7.834 1
*
*htstr s. type s. mult left heat right heat ht str no.
14662701 0 0 0 0
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
14662801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
14662901 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1

```

```

*****
$ wrapper, above transition cone
$
$ ht str no. 4701 wrapper,3
*****
*htstr ht str n pts geom init l.coord refl b.vol axl incr
14701000 1 4 2 1 5.264 0
*
*htstr mesh loch mesh fat
14701100 0 1

```

```

*
*htstr intervals rl_coord
1470100 3 5.296
*
*htstr compxn no. interval
1470120 2 3
*
*htstr source interval
1470130 0.0 3
*
*htstr temp mesh pt.
1470140 512.53 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
1470150 470010000 0 1 1 4.405 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
1470160 450010000 0 1 1 4.405 1
*
*htstr s. type s. mult left heat right heat ht str no.
1470170 0 0 0 0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
1470180 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
1470190 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$*****$
$wrapper around primary (swirl vane) separator $
$-----$
$ ht str no. 4741 wrapper.4 $
$-----$
*htstr ht str's w pts geom init l.coord refl b.vol axl incr
1474100 1 4 2 1 5.5888 0
*
*htstr mesh loch mesh fat
1474110 0 1
*
*htstr intervals rl_coord
1474120 3 5.6200
*
*htstr compxn no. interval
1474130 2 3
*
*htstr source interval
1474140 0.0 3
*
*htstr temp mesh pt.
1474150 517.89 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
1474160 474010000 0 1 1 7.98 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
1474170 454010000 0 1 1 7.98 1
*
*htstr s. type s. mult left heat right heat ht str no.
1474180 0 0 0 0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
1474190 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*

```

```

*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
1474200 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$*****$
$primary separator (swirl vane) $
$-----$
$ ht str no. 4742 swirl vane $
$-----$
*htstr ht str's w pts geom init l.coord refl b.vol axl incr
1474210 1 4 1 1 0.0 0
*
*htstr mesh loch mesh fat
1474220 0 1
*
*htstr intervals rl_coord
1474230 3 0.03125
*
*htstr compxn no. interval
1474240 2 3
*
*htstr source interval
1474250 0.0 3
*
*htstr temp mesh pt.
1474260 517.89 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
1474270 474010000 0 1 0 847.7 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
1474280 474010000 0 1 0 847.7 1
*
*htstr s. type s. mult left heat right heat ht str no.
1474290 0 0 0 0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
1474300 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
1474310 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
$*****$
$egg shell, elevation of dryer $
$-----$
$ ht str no. 4781 shell.5 $
$-----$
*htstr ht str's w pts geom init l.coord refl b.vol axl incr
1478100 1 6 2 1 6.59 0
*
*htstr mesh loch mesh fat
1478110 4541 1
*
*htstr temp flg
1478120 4541
*
*htstr left vol incr b.cond sa code area/factor ht str no.
1478130 478010000 0 1 1 5.20 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
1478140 0 0 0 1 5.20 1
*
*htstr s. type s. mult left heat right heat ht str no.
1478150 0 0 0 0 1
*

```

```

*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
14781801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
$-----$
$secondary separator (dryer vanes)
$
$ ht str no. 4782 dryer
$-----$
*htstr ht str's n pts geom init l.coord refl b.vol axl incr
14782000 1 4 1 1 0.0 0
*
*htstr mesh locn mesh fct
14782100 0 1
*
*htstr intervals rt coord
14782101 3 0.02083
*
*htstr compxn no. interval
14782201 2 3
*
*htstr source interval
14782301 0.0 3
*
*htstr temp mesh pt.
14782401 517.77 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
14782501 478010000 0 1 0 2347. 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
14782601 478010000 0 1 0 2347. 1
*
*htstr s. type s. mult left heat right heat ht str no.
14782701 0 0 0 0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
14782801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
14782901 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
$-----$
$sg shell, at elevation of dryer, including ellipsoidal top cap
$
$ ht str no. 4821 shell,6
$-----$
*htstr ht str's n pts geom init l.coord refl b.vol axl incr
14821000 1 6 1 1 6.59 0
*
*htstr mesh locn mesh fct
14821100 0 1
*
*htstr intervals rt coord
14821101 5 6.8817
*
*htstr compxn no. interval
14821201 2 5
*
*htstr source interval
14821301 0.0 5
*
*htstr temp mesh pt.
14821401 518.92 6

```

```

*htstr left vol incr b.cond sa code area/factor ht str no.
14821501 482010000 0 1 1 7.781 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
14821601 0 0 0 1 7.781 1
*
*htstr s. type s. mult left heat right heat ht str no.
14821701 0 0 0 0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
14821801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1
$-----$
$main feed line piping heat structures - from main feedwater header
$to each steam generator.
$-----$
$ ht str no. 5201 line a
$-----$
$line a heat structure modelling
$
*htstr ht str's n pts geom init l.coord refl b.vol axl incr
15201000 2 4 2 0 0.6808 0
*
*htstr mesh locn mesh fct
15201100 0 1
*
*htstr intervals rt coord
15201101 3 0.6867
*
*htstr compxn no. interval
15201201 2 3
*
*htstr source interval
15201301 0 3
*
*htstr temp mesh pt.
15201401 437.03 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
15201501 520010000 0 1 1 162.5 1
15201602 520010000 0 1 1 165.8539 2
*
*htstr right vol incr b.cond sa code area/factor ht str no.
15201601 0 0 0 1 162.5 1
15201602 0 0 0 1 165.8539 2
*
*htstr s. type s. mult left heat right heat ht str no.
15201701 0 0 0 0 2
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
15201801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 2
$-----$
$heat structures for the main steam line from steam generator to
$the steam header.
$-----$
$ ht str no. 5501 line a
$-----$
*htstr ht str's n pts geom init l.coord refl b.vol axl incr
15501000 2 4 2 0 0.7621 0
*
*htstr mesh locn mesh fct
15501100 0 1

```



```

*htstr intervals rt_coord
1550101 3 1.0833
*
*htstr compn no. interval
15501201 2 3
*
*htstr source interval
15501301 0 3
*
*htstr temp fig
15501401 0
*
*htstr temp mesh pt.
15501401 509.5 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
15501501 550010000 0 1 1 274.8631 1
15501502 580010000 0 1 1 20.0000 2
*
*htstr right vol incr b.cond sa code area/factor ht str no.
15501601 0 0 0 1 274.8631 1
15501602 0 0 0 1 20.0000 2
*
*htstr s. type s. mult left heat right heat ht str no.
15501701 0 0 0 0 1
15501702 0 0 0 0 2
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
15501801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 2
*
$*****
$ ht str no. 6201 line b
$-----
$efw line b heat structure modeling
$-----
*htstr ht str s pts geom init l.coord refl b.vol axl incr
16201000 2 4 2 0 0.5808 0
*
*htstr mesh loch mesh fat
16201100 0 1
*
*htstr intervals rt_coord
16201101 3 0.6667
*
*htstr compn no. interval
16201201 2 3
*
*htstr source interval
16201301 0 3
*
*htstr temp mesh pt.
16201401 437.07 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
16201501 610010000 0 1 1 178.0 1
16201502 620010000 0 1 1 59.1809 2
*
*htstr right vol incr b.cond sa code area/factor ht str no.
16201601 0 0 0 1 178.0 1
16201602 0 0 0 1 59.1809 2
*
*htstr s. type s. mult left heat right heat ht str no.
16201701 0 0 0 0 2

```

```

16201701 0 0 0 0 2
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
16201801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 2
*
$*****
$ heat structures for main steam line b - from steam generator b to
$steam header
$-----
*htstr ht str s pts geom init l.coord refl b.vol axl incr
16501000 2 4 2 1 0.9924 0
*
*htstr mesh loch mesh fat
16501100 0 1
*
*htstr intervals rt_coord
16501101 3 1.0833
*
*htstr compn no. interval
16501201 2 3
*
*htstr source interval
16501301 0 3
*
*htstr temp fig
16501401 0
*
*htstr temp mesh pt.
16501401 509.5 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
16501501 650010000 0 1 1 188.1638 1
16501502 660010000 0 1 1 20.0000 2
*
*htstr right vol incr b.cond sa code area/factor ht str no.
16501601 0 0 0 1 188.1638 1
16501602 0 0 0 1 20.0000 2
*
*htstr s. type s. mult left heat right heat ht str no.
16501701 0 0 0 0 2
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
16501801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 2
*
$*****
$ ht str no. 7001 line c
$-----
$efw line c heat structure modeling
$-----
*htstr ht str s pts geom init l.coord refl b.vol axl incr
17201000 2 4 2 0 0.5808 0
*
*htstr mesh loch mesh fat
17201100 0 1
*
*htstr intervals rt_coord
17201101 3 0.6667
*
*htstr compn no. interval
17201201 2 3
*
*htstr source interval
17201301 0 3
*

```

```

*htstr      temp      mesh pt.
17201401    437.06      4
*
*htstr      left vol   incr b.cond  sa code  area/factor  ht str no.
17201501    710010000  0      1      1      265.1055     1
17201502    720010000  0      1      1      54.25        2
*
*htstr      right vol  incr b.cond  sa code  area/factor  ht str no.
17201601    0           0      0      1      265.1055     1
17201602    0           0      0      1      54.25        2
*
*htstr      s. type   s. mult    left heat  right heat   ht str no.
17201701    0           0          0          0            2
*
*crdno     equiv diam heated len's  grid len's  grid cf's bf ht str no.
17201801    0           99.0  99.0  0.0  0.0  0.0  0.0 1.0 2
*
$*****$
$heat structures for steam line c - from steam generator c to steam hdr$
$*****$
*htstr      ht str  # pts  geom  init  l.coord  refl  b.vol  axl  incr
17501000    2      4      2      1      0.9924  0
*
*htstr      mesh loch   mesh fat
17501100    0           1
*
*htstr      intervals   rt. coord
17501101    3           1.0833
*
*htstr      compsn no.   interval
17501201    2           3
*
*htstr      source       interval
17501301    0.0         3
*
*htstr      temp fig
17501400    0
*
*htstr      temp      mesh pt.
17501401    509.50      4
*
*htstr      left vol   incr b.cond  sa code  area/factor  ht str no.
17501501    750010000  0      1      1      254.6617     1
17501502    760010000  0      1      1      20.0000      2
*
*htstr      right vol  incr b.cond  sa code  area/factor  ht str no.
17501601    0           0      0      1      254.6617     1
17501602    0           0      0      1      20.0000      2
*
*htstr      s. type   s. mult    left heat  right heat   ht str no.
17501701    0           0          0          0            2
*
*crdno     equiv diam heated len's  grid len's  grid cf's bf ht str no.
17501801    0           99.0  99.0  0.0  0.0  0.0  0.0 1.0 2
*
$*****$
$ steam header heat structure
$*****$
*htstr      ht str  # pts  geom  init  l.coord  refl  b.vol  axl  incr
18001050    1      4      2      1      2.7729  0
*
*htstr      mesh loch   mesh fat
18001100    0           1

```

```

*
*htstr      intervals   rt. coord
18001101    3           3.0021
*
*htstr      compsn no.   interval
18001201    2           3
*
*htstr      source       interval
18001301    0.0         3
*
*htstr      temp fig
18001400    0
*
*htstr      temp      mesh pt.
18001401    508.91      4
*
*htstr      left vol   incr b.cond  sa code  area/factor  ht str no.
18001501    800010000  0      1      1      15.00        1
*
*htstr      right vol  incr b.cond  sa code  area/factor  ht str no.
18001601    0           0      0      1      15.00        1
*
*htstr      s. type   s. mult    left heat  right heat   ht str no.
18001701    0           0          0          0            1
*
*crdno     equiv diam heated len's  grid len's  grid cf's bf ht str no.
18001801    0           99.0  99.0  0.0  0.0  0.0  0.0 1.0 1
*
$*****$
$heat structure for piping between steam header and turbine stop valves$
$*****$
*htstr      ht str  # pts  geom  init  l.coord  refl  b.vol  axl  incr
18021090    1      4      2      1      1.2313  0
*
*htstr      mesh loch   mesh fat
18021100    0           1
*
*htstr      intervals   rt. coord
18021101    3           1.3333
*
*htstr      compsn no.   interval
18021201    2           3
*
*htstr      source       interval
18021301    0.0         3
*
*htstr      temp fig
18021400    0
*
*htstr      temp      mesh pt.
18021401    507.03      4
*
*htstr      left vol   incr b.cond  sa code  area/factor  ht str no.
18021501    802010000  0      1      1      256.7220     1
*
*htstr      right vol  incr b.cond  sa code  area/factor  ht str no.
18021601    0           0      0      1      256.7220     1
*
*htstr      s. type   s. mult    left heat  right heat   ht str no.
18021701    0           0          0          0            1
*
*crdno     equiv diam heated len's  grid len's  grid cf's bf ht str no.
18021801    0           99.0  99.0  0.0  0.0  0.0  0.0 1.0 1
*

```

```

*****
Condensate and main feedwater piping heat structures
*****
$
ht str no. 8301          lp htr 1
$
-----
l.p. heaters 1 and 2 - heat structures represents only the tube with
an internal heat source representing the total
heat transferred per heater set at full power.
-----
*htstr ht str# n pts geom init l.coord refl b.vol axl incr
18301000 1 4 2 0 0.0220 0
*
*htstr mesh locn mesh fat
18301100 0 1
*
*htstr intervals rt coord
18301101 3 0.0260
*
*htstr compxn no. interval
18301201 1 3
*
*htstr source interval
18301301 1.0 3
*
*htstr temp mesh pt.
18301401 174.02 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
18301501 830010000 0 1 1 220990.0 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
18301601 0 0 0 1 220990.0 1
*
*htstr s. type s. mult left heat right heat ht str no.
18301701 10870 1.1625e+08 0.0 0.0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
18301801 0 89.0 89.0 0.0 0.0 0.0 0.0 1.0 1
*
*****
$
ht str no. 8302          lp htr 2
$
-----
*htstr ht str# n pts geom init l.coord refl b.vol axl incr
18302000 1 4 2 0 0.0272 0
*
*htstr mesh locn mesh fat
18302100 0 1
*
*htstr intervals rt coord
18302101 3 0.0313
*
*htstr compxn no. interval
18302201 2 3
*
*htstr source interval
18302301 1.0 3
*
*htstr temp mesh pt.
18302401 205.57 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
18302501 83002000 0 1 1 104494.570 1

```

```

*
*htstr right vol incr b.cond sa code area/factor ht str no.
18302601 0 0 0 1 104494.570 1
*
*htstr s. type s. mult left heat right heat ht str no.
18302701 10870 7.2674e+07 0.0 0.0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
18302801 0 89.0 89.0 0.0 0.0 0.0 0.0 1.0 1
*
*****
$
ht str no. 8341          htr conn p
$
-----
Piping connecting l.p. heaters 2 and 3
-----
*htstr ht str# n pts geom init l.coord refl b.vol axl incr
18341000 1 4 2 0 0.0286 0
*
*htstr mesh locn mesh fat
18341100 0 1
*
*htstr intervals rt coord
18341101 3 0.0290
*
*htstr compxn no. interval
18341201 2 3
*
*htstr source interval
18341301 0.0 3
*
*htstr temp mesh pt.
18341401 201.01 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
18341501 834010000 0 1 1 234.4498 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
18341601 0 0 0 1 234.4498 1
*
*htstr s. type s. mult left heat right heat ht str no.
18341701 0 0 0 0 0 1
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
18341801 0 89.0 89.0 0.0 0.0 0.0 0.0 1.0 1
*

```

```

*****
$
ht str no. 8401          lp htr 3
$
-----
l.p. heaters 3,4 and 5 and piping between l.p. heater 5 and pump
suction header. only the tubes are modeled in the heaters.
-----
*htstr ht str# n pts geom init l.coord refl b.vol axl incr
18401000 1 4 2 0 0.0237 0
*
*htstr mesh locn mesh fat
18401100 0 1
*
*htstr intervals rt coord
18401101 3 0.0200
*
*htstr compxn no. interval
18401201 2
*
*htstr source interval

```

```

18401301      1.0          3
*htstr      1-mp          mesh pt.
18401401      261.02         4
*
*htstr      left vol      incr b.cond sa code area/factor ht str no.
18401501      84001700      0      1      1      157658.743      1
*
*htstr      right vol     incr b.cond sa code area/factor ht str no.
18401601      0      0      0      1      157658.743      1
*
*htstr      s. type      s. mult      left heat      right heat      ht str no.
18401701      10070      1.1450e+08      0.0      0.0      1
*
*ordno      equiv diam      heated len's      grid len's      grid cf's bf ht str no.
18401801      0      99.0      99.0      0.0      0.0      0.0      0.0      1.0      1
*
$-----$
$      ht str no. 8402      pmp scin
$-----$
*htstr      ht str's      n pts      geom      init      l.coord      refl      b.vol      axl. incr
18402000      2      4      2      0      0.0232      0
*
*htstr      mesh loch      mesh fat
18402100      0      1
*
*htstr      intervals      rt. coord
18402101      3      0.0313
*
*htstr      compxn no.      interval
18402201      1      3
*
*htstr      source      interval
18402301      1.0      3
*
*htstr      temp      mesh pt.
18402401      375.96      4
*
*htstr      left vol      incr b.cond sa code area/factor ht str no.
18402501      840020000      0      1      1      118777.870      1
18402502      840030000      0      1      1      102432.000      2
*
*htstr      right vol     incr b.cond sa code area/factor ht str no.
18402601      0      0      0      1      118777.870      1
18402602      0      0      0      1      102432.000      2
*
*htstr      s. type      s. mult      left heat      right heat      ht str no.
18402701      10870      1.1272e+08      0.0      0.0      1
18402702      10870      1.3399e+08      0.0      0.0      2
*
*ordno      equiv diam      heated len's      grid len's      grid cf's bf ht str no.
18402801      0      99.0      99.0      0.0      0.0      0.0      0.0      1.0      2
*
$-----$
$      ht str no. 8801      pmp scin
$-----$
Main feedwater pump suction piping heat structure
$-----$
*htstr      ht str's      n pts      geom      init      l.coord      refl      b.vol      axl. incr
18601000      1      4      2      0      1.3196      0
*
*htstr      mesh loch      mesh fat
18601100      0      1

```

```

*
*htstr      intervals      rt. coord
18601101      3      1.1923
*
*htstr      compxn no.      interval
18601201      2      3
*
*htstr      source      interval
18601301      0.0      3
*
*htstr      temp      mesh pt.
18601401      369.87      4
*
*htstr      left vol      incr b.cond sa code area/factor ht str no.
18601501      860010000      0      1      1      241.0039      1
*
*htstr      right vol     incr b.cond sa code area/factor ht str no.
18601601      0      0      0      1      241.5039      1
*
*htstr      s. type      s. mult      left heat      right heat      ht str no.
18601701      0      0      0      0      0      1
*
*ordno      equiv diam      heated len's      grid len's      grid cf's bf ht str no.
18601801      0      99.0      99.0      0.0      0.0      0.0      0.0      1.0      1
*
$-----$
$      ht str no. 862      pmp disch line a
$-----$
$mfw pump outlet piping
$-----$
*htstr      ht str's      n pts      geom      init      l.coord      refl      b.vol      axl. incr
18621000      1      4      2      0      0.7266      0
*
*htstr      mesh loch      mesh fat
18621100      0      1
*
*htstr      intervals      rt. coord
18621101      3      0.6333
*
*htstr      compxn no.      interval
18621201      2      3
*
*htstr      source      interval
18621301      0.0      3
*
*htstr      temp      mesh pt.
18621401      370.64      4
*
*htstr      left vol      incr b.cond sa code area/factor ht str no.
18621501      862010000      0      1      1      50.0      1
*
*htstr      right vol     incr b.cond sa code area/factor ht str no.
18621601      0      0      0      1      50.0      1
*
*htstr      s. type      s. mult      left heat      right heat      ht str no.
18621701      0      0      0      0      0      1
*
*ordno      equiv diam      heated len's      grid len's      grid cf's bf ht str no.
18621801      0      99.0      99.0      0.0      0.0      0.0      0.0      1.0      1
*
$-----$
$      ht str no. 805      pmp disch line b
$-----$
$mfw pump outlet piping
$

```

```

*htstr ht str n pts geom init l.coord refl b.vol axl incr
18651000 1 4 2 0 0.7266 0
*
*htstr mesh loch mesh fat
18651100 0 1
*
*htstr intervals rt.coord
18651101 3 0.8333
*
*htstr compn no. interval
18651201 2 3
*
*htstr source interval
18651301 0.0 3
*
*htstr temp mesh pt.
18651401 370.84 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
18651501 885010000 0 1 1 50.0 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
18651601 0 0 0 1 50.0 1
*
*htstr s. type s. mult left heat right heat ht str no.
18651701 0 0 0 0
*
*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
18651801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1

```

```

$*****$
$ ht str no. 867 pmp disch combined lines $
$

```

```

$mfw pump outlet piping $

```

```

*htstr ht str n pts geom init l.coord refl b.vol axl incr
18671000 1 4 2 0 1.0275 0
*
*htstr mesh loch mesh fat
18671100 0 1
*
*htstr intervals rt.coord
18671101 3 1.1343
*
*htstr compn no. interval
18671201 2 3
*
*htstr source interval
18671301 0.0 3
*
*htstr temp mesh pt.
18671401 370.84 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
18671501 807010000 0 1 1 48.0 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
18671601 0 0 0 1 48.0 1
*
*htstr s. type s. mult left heat right heat ht str no.
18671701 0 0 0 0

```

```

*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
18671801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1

```

```

$*****$
$ ht str no. 8741 no htr $
$

```

```

$sh.p. heater heat structure modeling $

```

```

*htstr ht str n pts geom init l.coord refl b.vol axl incr
18741000 1 4 2 0 0.0231 0
*
*htstr mesh loch mesh fat
18741100 0 1
*
*htstr intervals rt.coord
18741101 3 0.0290
*
*htstr compn no. interval
18741201 1 3
*
*htstr source interval
18741301 1.0 3
*
*htstr temp mesh pt.
18741401 444.20 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
18741501 374010000 0 1 1 23070.0 1
*
*htstr right vol incr b.cond sa code area/factor ht str no.
18741601 0 0 0 1 23070.0 1
*
*htstr s. type s. mult left heat right heat ht str no.
18741701 10870 2.1338e+68 0.0 0.0 1

```

```

*crdno equiv diam heated len's grid len's grid cf's bf ht str no.
18741801 0 99.0 99.0 0.0 0.0 0.0 0.0 1.0 1

```

```

$*****$
$ ht str no. 8781 header $
$

```

```

$sh.p. heater outlet piping and mfw header $

```

```

*htstr ht str n pts geom init l.coord refl b.vol axl incr
18781000 1 4 2 0 1.0275 0
*
*htstr mesh loch mesh fat
18781100 0 1
*
*htstr intervals rt.coord
18781101 3 1.1343
*
*htstr compn no. interval
18781201 2 3
*
*htstr source interval
18781301 0.0 3
*
*htstr temp mesh pt.
18781401 437.44 4
*
*htstr left vol incr b.cond sa code area/factor ht str no.
18781501 878010000 0 1 1 46.6815 1

```



\*htstr right vol incr b-load ss code area/factor ht str no.  
18781601 0 0 0 1 46.6815 1

\*htstr s. type s. mult left heat right heat ht str no.  
18781701 0 0 0 0 1

\*cardno equiv diam heated len's grid len's grid cf's bf ht str no.  
18781801 0 2.0 99.0 0.0 0.0 0.0 0.0 1.0 1

\*\*\*\*\*  
\$  
\$ material properties \$  
\$  
\*\*\*\*\*

\* all conductivity values are in units of btu/sec-ft-degf  
\* all volumetric heat capacity values are in btu/ft<sup>3</sup>-degf

\*\*\*\*\*  
\* thermal properties of ss-3161 - composition 1 \*  
\*\*\*\*\*

\*cardno mtrl type th.con ht.cap material  
20100100 1 1 \* ss-3161

\* thermal properties of ss-3161

\*cardno temperature th.con  
20100101 32.0 0.00215  
20100102 100.0 0.00215  
20100103 800.0 0.00396  
20100104 1600.0 0.00397  
20100105 3600.0 0.00397

\*cardno temperature vol ht cap  
20100151 32.0 61.30  
20100152 800.0 61.30  
20100153 800.0 64.60  
20100154 800.0 67.10  
20100155 1000.0 69.35  
20100156 4000.0 69.35

\*\*\*\*\*  
\* thermal properties of carbon steel - composition 2 \*  
\*\*\*\*\*

\*cardno mtrl type th.con ht.cap material  
20100200 1 1 \* carbon steel

\* thermal properties of carbon steel

\*cardno temperature th.con  
20100201 32.0 0.01126  
20100202 80.0 0.01126  
20100203 440.33 0.01009  
20100204 800.33 0.00908  
20100205 1160.33 0.00824  
20100206 1520.33 0.00750  
20100207 1880.33 0.00705

20100208 2240.33 0.00670  
20100209 2600.33 0.00652  
20100210 3000.33 0.00640

\*cardno temperature vol ht cap  
20100251 32.00 57.29  
20100252 80.00 57.29  
20100253 200.03 57.20  
20100254 1600.07 82.04  
20100255 2600.33 104.71  
20100256 2960.33 112.49

\*\*\*\*\*  
\* thermal properties of inconel 600 - composition 3 \*  
\*\*\*\*\*

\*cardno mtrl type th.con ht.cap material  
20100300 1 1 \* inconel 600

\* thermal properties of inconel 600

\*cardno temperature th.con  
20100301 100.0 0.00236  
20100302 300.0 0.00267  
20100303 500.0 0.00294  
20100304 700.0 0.00322  
20100305 900.0 0.00350  
20100306 1100.0 0.00378

\*cardno temperature vol ht cap  
20100351 52.525

\*\*\*\*\*  
\* thermal properties of cladding - composition 4 \*  
\*\*\*\*\*

\*cardno mtrl type th.con ht.cap material  
20100400 1 1 \* cladding

\* thermal properties of cladding

\*cardno temperature th.con  
20100401 32 1.9257e-3  
20100402 292.0 1.9257e-3  
20100403 512.0 2.2470e-3  
20100404 1112.0 2.2937e-3  
20100405 1472.0 3.0469e-3  
20100406 1832.0 3.5225e-3  
20100407 2192.0 4.0142e-3  
20100408 2552.0 4.6100e-3  
20100409 2912.0 5.2205e-3  
20100410 3272.0 7.0647e-3  
20100411 3632.0 8.2114e-3  
20100412 3992.0 1.0910e-2

\*cardno temperature vol ht cap  
20100451 0 0 29.292  
20100452 1480 3 34.476  
20100453 1875 0 65.176  
20100454 267.5 34.370  
20100455 3500 0 34.476

\* thermal properties of uo2 - composition 5 \*

\*crdno mtrl type th.con ht.cap material  
20100500 tbi/fctn 1 1 \* uo2

thermal properties of uo2

*crdno	temperature	th.cond
20100501	32.0	1.294e-3
20100502	100.0	1.294e-3
20100503	332.0	1.125e-3
20100504	440.0	9.951e-4
20100505	500.0	9.2806e-4
20100506	650.0	7.4194e-4
20100507	800.0	7.4361e-4
20100508	897.0	5.9390e-4
20100509	1104.0	5.2310e-4
20100510	1213.0	4.9200e-4
20100511	1326.0	4.6710e-4
20100512	1684.0	4.4700e-4
20100513	1700.0	4.4701e-4
20100514	1850.0	4.5528e-4
20100515	2000.0	4.3556e-4
20100516	2150.0	4.1861e-4
20100517	2300.0	4.0472e-4
20100518	2450.0	3.9308e-4
20100519	2600.0	3.8389e-4
20100520	3100.0	3.6750e-4
20100521	3600.0	3.7828e-4
20100522	4100.0	3.9056e-4
20100523	4600.0	4.2722e-4
20100524	5100.0	4.8050e-4

*crdno	temperature	vol. ht.cap
20100551	32.0	54.45
20100552	122.0	38.25
20100553	212.0	40.95
20100554	362.0	43.55
20100555	752.0	46.80
20100556	2012.0	51.25
20100557	2732.0	52.85
20100558	3082.0	56.55
20100559	3452.0	63.05
20100560	3812.0	72.80
20100561	4152.0	80.70
20100562	4532.0	94.25
20100563	4712.0	98.15
20100564	4892.0	100.10
20100565	5144.0	101.40
20100566	8000.0	101.40

\* thermal properties of fuel gap(average core) - composition 6 \*

\*crdno mtrl type th.con ht.cap material  
20100600 tbi/fctn 1 1 \* fuel gap

thermal properties of fuel gap

*crdno	temperature	th.cond
20100601	32.0	0.00031
20100602	5400.0	0.00031

*crdno	temperature	vol. ht.cap
20100651	32.0	0.00031
20100652	5400.0	0.00031

\* thermal properties of air - composition 7 \*

\*crdno mtrl type th.con ht.cap material  
20100700 tbi/fctn 1 1 \* air

thermal properties of air

*crdno	temperature	th.cond
20100701	80.0	4.222e-6
20100702	100.0	4.333e-6
20100703	150.0	4.639e-6
20100704	200.0	4.972e-6
20100705	250.0	5.306e-6
20100706	300.0	5.639e-6
20100707	400.0	6.250e-6
20100708	500.0	6.833e-6
20100709	600.0	7.500e-6
20100710	800.0	8.417e-6
20100711	1000.0	9.361e-6
20100712	1500.0	1.130e-5

*crdno	tempert	vol. ht.cap
20100751	80.0	0.0176
20100752	100.0	0.0170
20100753	150.0	0.0157
20100754	200.0	0.0145
20100755	250.0	0.0135
20100756	300.0	0.0127
20100757	400.0	0.0113
20100758	500.0	0.0102
20100759	600.0	9.3874e-2
20100760	800.0	8.0955e-2
20100761	1000.0	7.1536e-2
20100762	1500.0	5.6231e-2

\* thermal properties of HgO(pvc heaters) - composition 8 \*

\*crdno mtrl type th.con ht.cap material  
20100800 tbi/fctn 1 1 \* HgO

thermal properties of HgO

*crdno	temperature	th.cond
20100801	65.09	0.0001324
20100802	1932.09	0.0001703

*crdno	temperature	vol. ht.cap
20100851	250.3	42.31

\*\*\*\*\*  
 \$ general table  
 \*\*\*\*\*

\*\*\*\*\*  
 \$ core power and power decay table  
 \*\*\*\*\*

*crdno	table type	trip no.	factor 1	factor 2	factor 3
20210000	power	000	1.0	2300.00	

\*Decay power table

**card	sec	normalized power
20210001	1.	1.0
20210002	0.	1.0
20210003	0.11717	0.99166
20210004	0.20882	0.97301
20210005	0.24143	0.95763
20210006	0.26321	0.94534
20210007	0.28517	0.92990
20210008	0.30704	0.91853
20210009	0.32813	0.90412
20210010	0.34932	0.87520
20210011	0.37099	0.85392
20210012	0.40163	0.83010
20210013	0.41618	0.81372
20210014	0.43067	0.79545
20210015	0.45971	0.76110
20210016	0.50334	0.71526
20210017	0.53968	0.67173
20210018	0.56860	0.61968
20210019	0.58307	0.58592
20210020	0.61183	0.53450
20210021	0.65542	0.47910
20210022	0.68896	0.42724
20210023	0.74981	0.37056
20210024	0.82253	0.29188
20210025	0.88958	0.23361
20210026	0.93890	0.18983
20210027	0.98267	0.15209
20210028	1.04833	0.12004
20210029	1.15803	0.10058
20210030	1.47289	0.07646
20210031	1.63910	0.06706
20210032	2.23468	0.05131
20210033	2.52793	0.04776
20210034	3.04782	0.03510
20210035	3.41411	0.03298
20210036	3.80968	0.04968
20210037	4.25654	0.04651
20210038	4.62283	0.04530
20210039	5.01111	0.04465
20210040	5.58253	0.04327
20210041	6.03673	0.04182
20210042	6.80815	0.03969
20210043	7.37734	0.03624
20210044	7.78627	0.03485
20210045	100.	0.0271
20210046	400.	0.0235

20210047	800.	0.0186
20210048	1000.	0.0185
20210049	2000.	0.0157
20210050	4000.	0.0129
20210051	8000.	0.0105
20210052	10000.	0.00965
20210053	20000.	0.00795
20210054	60000.	0.00566
20210055	100000.	0.00475

\*\*\*\*\*  
 \$ table no. 107 - # loops sp  
 \*\*\*\*\*

*table	table type	trip no.	factor 1	factor 2
20219700	react			
*table		time		reactivity
20219701		0.09999		4.0
20219702		0.10		2.0
20219703		0.39999		2.0
20219704		0.40		1.0

\*\*\*\*\*  
 \$ table no. 500 - sfty dif.  
 \*\*\*\*\*

*table	table type	trip no.	factor 1	factor 2
20250000	react			
*table		time		power
20250001		1041.59999		0.0
20250002		1041.60000		0.187
20250003		1050.79999		0.172
20250004		1050.80000		0.139
20250005		1079.99999		0.148
20250006		1080.00000		0.500
20250007		1084.99999		0.594
20250008		1085.00000		0.464
20250009		1094.79999		0.470
20250010		1094.80000		0.712
20250011		1104.99999		0.854
20250012		1105.00000		0.854
20250013		1124.99999		0.604
20250014		1125.00000		0.415
20250015		1139.99999		0.422
20250016		1140.00750		0.234
20250017		1193.49999		0.242
20250018		1193.50700		0.187
20250019		1215.49999		0.193
20250020		1215.50000		0.128
20250021		1227.49999		0.183
20250022		1227.50000		0.959
20250023		1254.00000		0.081

\*\*\*\*\*  
 \$ table no. 501 - sfty low  
 \*\*\*\*\*

*table	table type	no.	factor 1	factor 2
20250100	react			
*table		time		power
20250101		1041.59999		0.0
20250102		1041.60000		0.0
20250103		1050.79999		0.0
20250104		1050.80000		0.0
20250105		1079.99999		0.0

20250100	1080.00000	0.0
20250101	1084.99999	0.0
20250102	1089.00000	0.130
20250103	1094.29999	0.132
20250104	1094.40000	0.132
20250105	1104.99999	0.133
20250106	1105.00000	0.263
20250107	1124.99999	0.270
20250108	1125.00000	0.459
20250109	1139.99999	0.467
20250110	1140.00000	0.655
20250111	1180.99999	0.659
20250112	1193.50000	0.754
20250113	1215.49999	0.769
20250114	1215.50000	0.874
20250115	1227.49999	0.835
20250116	1227.50000	0.915
20250117	1254.00000	0.919

table no. 808 - steam dump n

*table	table type	trip no.	factor 1	factor 2
20280800	normarea			

*table	length	area
20280801	0.0	0.0000
20280802	0.2	0.2005
20280803	0.4	0.4002
20280804	0.6	0.6002
20280805	0.8	0.8002
20280806	1.0	1.0000

table no. 900 - trip table

*table	table type	trip no.	factor 1	factor 2
20290000	reas-1			

*table	time	reactivity
20290001	-1.0e-99	0.0
20290002	0.0	1.0

control system

The first two control variables calculate the time step size.

*ctivar	name	type	factor	init	f c
20500100	'time ste'	sum	1.0	0.0	0

*ctivar	ad	coeff	variable name	parameter no.
20500101	0.0	1.0	time	0
20500102		-1.0	ctrlvar	002

*ctivar	name	type	factor	init	f c
20500200	'last tim'	mult	1.0	0.0	0

20500201 time 0

steam generator, total mass inventory, lbs

*ctivar	name	type	factor	init	f c
20500300	'sg mass'	sum	2.2	93260.0	0 0

*ctivar	ad	coeff	variable name	parameter no.
20500301	0.0	15.52	rho	25410000
20500302		5.11	rho	25610000
20500303		3.98	rho	262010000
20500304		1.28	rho	262020000
20500305		1.26	rho	262030000
20500306		0.97	rho	262040000
20500307		7.90	rho	266010000
20500308		10.26	rho	266020000
20500309		10.40	rho	266030000
20500310		10.74	rho	266040000
20500311		10.73	rho	270010000
20500312		14.17	rho	274010000
20500313		19.75	rho	278010000
20500314		19.68	rho	282010000

steam generator b

*ctivar	name	type	factor	init	f c
20500500	'sg mass'	sum	2.2	93260.0	0 0

*ctivar	ad	coeff	variable name	parameter no.
20500501	0.0	15.52	rho	354010000
20500502		5.11	rho	354010000
20500503		3.98	rho	362010000
20500504		1.28	rho	362020000
20500505		1.26	rho	362030000
20500506		0.97	rho	362040000
20500507		7.90	rho	366010000
20500508		10.26	rho	366020000
20500509		10.40	rho	366030000
20500510		10.74	rho	366040000
20500511		10.73	rho	370010000
20500512		14.17	rho	374010000
20500513		19.75	rho	378010000
20500514		19.68	rho	382010000

steam generator c

*ctivar	name	type	factor	init	f c
20500700	'sg mass'	sum	2.2	93260.0	0 0

*ctivar	ad	coeff	variable name	parameter no.
20500701	0.0	15.52	rho	454010000
20500702		5.11	rho	454010000
20500703		3.98	rho	462010000
20500704		1.28	rho	462020000
20500705		1.26	rho	462030000
20500706		0.97	rho	462040000
20500707		7.90	rho	466010000
20500708		10.26	rho	466020000
20500709		10.40	rho	466030000
20500710		10.74	rho	466040000
20500711		10.73	rho	470010000

```

20500712 14.1 rhd #74010000
20500713 12.75 rhd #70010000
20500714 10.00 rhd #62010000
*.....*
the following control variables are used to prevent excessive cpu/real
time slices from occurring. the documentation is on page 112
*.....*
*clivar name type factor init f c
20501900 'cpu inir' sum 1.0 0.0 0
*
*clivar a0 coeff variable name parameter no.
20501901 0.0 1.0 ctrlivar 0
20501902 1.0 ctrlivar 028
*.....*
*clivar name type factor init f c
20502000 'intrvl e' sum 1.0 0.0 0
*
*clivar a0 coeff variable name parameter no.
20502001 -100.0 1.0 ctrlivar 01P
*.....*
*clivar name type factor init f c max max
20502100 'cp. trip' function 1.0e-05 1.0 0.2 1.7
*
*clivar brch arg. name brch arg. no. table no.
20502101 ctrlivar 026 #00
*.....*
*clivar name type factor init f c
20502200 'new bias' mult 1.0 0.0 1
*
*clivar variable name parameter no. variable name parameter no.
20502201 cpulime 0 ctrlivar 021
*.....*
*clivar name type factor init f c
20502300 'cpu ' bi' stdfnctn 1.0 0.0 1
*
*clivar function
20502301 max
*clivar variable name parameter no. variable name parameter no.
20502302 ctrlivar 022 ctrlivar 024
*.....*
*clivar name type factor init f c
20502400 'cpu bias' stdfnctn 1.0 1.0e5 0
*
*clivar function
20502401 min
*clivar variable name parameter no. variable name parameter no.
2050 02 cpulime 0 ctrlivar 023
*.....*
*clivar name type factor init f c
20502500 'tim inir' sum 1.0 1.0e-6 0 1 1. -
*
*clivar a0 coeff variable name parameter no.
20502501 0.0 1.0 time 0
20502502 -1.0 ctrlivar 027
*.....*
*clivar name type factor init f c
20502600 'new i bi' mult 1.0 0.0 1
*
*clivar variable name parameter no. variable name parameter no.
20502601 time 0 ctrlivar 021
*.....*
*clivar name type factor init f c
20502700 'time bias' stdfnctn 1.0 0.0 1

```

```

*
*clivar function
20502701 max
*clivar variable name parameter no. variable name parameter no.
20502702 ctrlivar 026 ctrlivar 027
*.....*
*clivar name type factor init f c
20502800 'cpu/real' div 1.0 0.0 0
*
*clivar divisor name divisor no. dividend name dividend no.
20502801 ctrlivar 026 ctrlivar 019
*.....*
*clivar name type factor init f c
20502900 'cpu real' mult 1.0 0.0 0
*
*clivar variable name pa meter no. variable name parameter no.
20502901 ctrlivar 021 ctrlivar 029
*.....*
the following set of control variables are used to stop the calcula
tion if the number of consecutive calculations at or below the user
specified time step size exceeds the desired number. documentation
can be found on pages 13-15.
*.....*
*clivar name type factor init f c
20503000 'min i er' sum 1.0 0.0 0
*
*clivar a0 coeff variable name parameter no.
20503001 1.0e-5 -1.0 ctrlivar 001
*.....*
*clivar name type factor init f c max max
20503100 'tim trip' function 1.0e-05 0.0 0.2 1.0
*
*clivar brch arg. name brch arg. no. table no.
20503101 ctrlivar 030 #00
*.....*
*clivar name type factor init f c
20503200 'i tip co' sum 1.0 1.0 0
*
*clivar a0 coeff variable name parameter no.
20503201 1.0 -1.0 ctrlivar 031
*.....*
*clivar name type factor init f c min
20503300 'i tip su' sum 1.0 0.0 0 1 0.0
*
*clivar a0 coeff variable name parameter no.
20503301 0.0 1.0 ctrlivar 031
20503302 1.0 ctrlivar 033
20503303 -1.0 ctrlivar 034
*.....*
*clivar name type factor init f c
20503400 'step bias' mult 1.0 0.0 0
*
*clivar variable name parameter no. variable name parameter no.
20503401 ctrlivar 032 ctrlivar 033
*.....*
the following control variables are used to regulate the top speed in $
the s/s initialization phase to obtain the desired primary loop flow. $
*.....*
*clivar name type factor init f c
20504000 'top s er' sum 2.2046 0.0 0
*
*clivar a0 coeff variable name parameter no.
20504001 12705.763 -1.0 mflow 120010000
20504002 -1.0 mflow 120020000

```



```

2050400 -1.0 wflow 12003000
*****
ctrlvar name type factor init f c min max
2050500 'rtp spec' integral 2.551e-2 1790.0 0.0 0.0 1200.0
*
ctrlvar integrand name integrand no.
2050501 ctrlvar 049
*****
the following control variable is core differential temperature
*****
ctrlvar name type factor init f c
2050600 'core dt' sum 1.8000 0.0 0
*
ctrlvar ab coeff variable name parameter no.
2050601 0.0 1.0 tempf 11001000
2050602 -1.0 tempf 11201000
*****
the following control variable is normalized reactor pm17. document-
ation is on page 16.
*****
ctrlvar name type factor init f c
2050700 'n r x pow' function 4.3479e-10 1.0 0
*
ctrlvar arch arg name arch arg no. table no.
2050801 time 0 100
*****
the following control variables calculate the primary average temp-
eratures. documentation is on pages 17-18.
*****
ctrlvar name type factor init f c
2050910 'a temp' sum 1.0 175.4 1
*
ctrlvar ab coeff variable name parameter no.
2050911 -659.07 0.0 tempf 20401000
2050912 0.0 tempf 21001000
*****
ctrlvar name type factor init f c
2050920 'b temp' sum 1.0 175.4 1
*
ctrlvar ab coeff variable name parameter no.
2050921 -659.07 0.0 tempf 24040000
2050922 0.0 tempf 21001000
*****
ctrlvar name type factor init f c
2050930 'c temp' sum 1.0 175.4 1
*
ctrlvar ab coeff variable name parameter no.
2050931 -659.07 0.0 tempf 40501000
2050932 0.0 tempf 41001000
*****
ctrlvar name type factor init f c
2050940 'high' 'v' stochastic 1.0 175.4 1
*
ctrlvar function
2050941 max
ctrlvar variable name parameter no. variable name parameter no.
2050942 ctrlvar 101 ctrlvar 102
2050943 ctrlvar 102
*****
the following control variables determine the number of loops that
have a temp in 543. if 2/3 (2 out of 3) loops have a low temp a
1/2 trip status is satisfied for whv closure. documentation is
on pages 19-20.
*****

```

```

*****
ctrlvar name type factor init f c
2051050 '543-atav' sum 1.0 0.0 0
*
ctrlvar ab coeff variable name parameter no.
2051051 543.0 -1.0 ctrlvar 101
*****
ctrlvar name type factor init f c max max
2051060 '543-btav' function 1.0e99 0.0 0.2 1.0
*
ctrlvar arch arg name arch arg no. table no.
2051061 ctrlvar 105 100
*****
ctrlvar name type factor init f c
2051070 '543-ctav' sum 1.0 0.0 0
*
ctrlvar ab coeff variable name parameter no.
2051071 543.0 -1.0 ctrlvar 102
*****
ctrlvar name type factor init f c max max
2051080 '543-dtav' function 1.0e99 0.0 0.2 1.0
*
ctrlvar arch arg name arch arg no. table no.
2051081 ctrlvar 101 100
*****
ctrlvar name type factor init f c
2051090 '543-etav' sum 1.0 0.0 0
*
ctrlvar ab coeff variable name parameter no.
2051091 543.0 -1.0 ctrlvar 103
*****
ctrlvar name type factor init f c max max
2051100 '543-ftav' function 1.0e99 0.0 0.2 1.0
*
ctrlvar arch arg name arch arg no. table no.
2051101 ctrlvar 102 100
*****
ctrlvar name type factor init f c
2051110 '543-gtav' sum 1.0 0.0 0
*
ctrlvar ab coeff variable name parameter no.
2051111 0.0 1.0 ctrlvar 105
2051112 1.0 ctrlvar 108
2051113 1.0 ctrlvar 110
*****
the following control variable calculates the setpoint average temp-
erature. documentation is on pages 21-22.
*****
ctrlvar name type factor init f c min max
2051150 '1ref' sum 1.0 175.4 1.3 140.0 215.0
*
ctrlvar ab coeff variable name parameter no.
2051151 140.224 7.45e-6 0 14001000
*****
the following control variables calculate the reactor out-temperature
and its trip status. documentation is on pages 23-25. the a loop
logic is in 127-128, the b and c loops control variables are 131-136
and 141-146, respectively.
*****
ctrlvar name type factor init f c
2051200 'a3ig-225' sum 7.47e-4 0.0 0
*

```

```

*clivar      a0      coeff      variable name parameter no.
2051200      -2250.0    1.85037e-4      0      040010000
*
*clivar      name      type      factor      init      f c
20512100 'a del te' sum      1.0      57.5      0
*
*clivar      a0      coeff      variable name parameter no.
20512101      0.0      1.0      temp1      204000000
20512102      -1.0      -1.0      temp1      216010000
*
*clivar      name      type      factor      init      f c
20512200 'atavg 57' sum      1.0      0.0      0
*
*clivar      a0      coeff      variable name parameter no.
20512201      -875.4      1.0      ctrlivar      101
*
*clivar      name      type      factor      init      f c
20512300 'a2(1-1)' lead-lag 0.01035 0.0      0
*
*clivar      tau-1      tau-2      variable name parameter no.
20512301      20.0      3.0      ctrlivar      122
*
*clivar      name      type      factor      init      f c
20512400 'brdel1 a' sum      57.5      0.0      0
*
*clivar      a0      coeff      variable name parameter no.
20512401      1.162      1.0      ctrlivar      120
20512402      -1.0      -1.0      ctrlivar      123
*
*clivar      name      type      factor      init      f c
20512500 'brdt-d10' sum      1.0      -1.0      0
*
*clivar      a0      coeff      variable name parameter no.
20512501      0.0      1.0      ctrlivar      121
20512502      -1.0      -1.0      ctrlivar      124
*
*clivar      name      type      factor      init      f c      max      max
20512600 'brdt-d10' function 1.0e99 0.0      0.2      1.0
*
*clivar      srch arg name      srch arg no.      table no.
20512601      ctrlivar      125      900
*
The following control variables calculate the turbine over temperature
delta 1 trip. control variables 127-129 represent the a loop, 127-130
and 147-149 represent the b and c loops, respectively. documentation
is on page 26.
*
*clivar      name      type      factor      init      f c
20512700 'b del te' sum      57.5      0.0      0
*
*clivar      a0      coeff      variable name parameter no.
20512701      1.152      1.0      ctrlivar      120
20512702      -1.0      -1.0      ctrlivar      123
*
*clivar      name      type      factor      init      f c
20512800 'b del te' sum      1.0      -1.0      0
*
*clivar      a0      coeff      variable name parameter no.
20512801      0.0      1.0      ctrlivar      121
20512802      -1.0      -1.0      ctrlivar      127
*
*clivar      name      type      factor      init      f c      max      max
20512900 'b del te' function 1.0e99 0.0      0.2      1.0

```

```

*
*clivar      srch arg name      srch arg no.      table no.
20512901      ctrlivar      128      900
*
*clivar      name      type      factor      init      f c
20513100 'b del te' sum      1.8      57.5      0
*
*clivar      a0      coeff      variable name parameter no.
20513101      0.0      1.0      temp1      204000000
20513102      -1.0      -1.0      temp1      206010000
*
*clivar      name      type      factor      init      f c
20513200 'btavg 57' sum      1.0      0.0      0
*
*clivar      a0      coeff      variable name parameter no.
20513201      -875.4      1.0      ctrlivar      102
*
*clivar      name      type      factor      init      f c
20513300 'b2(1-1)' lead-lag 0.01035 0.0      0
*
*clivar      tau-1      tau-2      variable name parameter no.
20513301      20.0      3.0      ctrlivar      132
*
*clivar      name      type      factor      init      f c
20513400 'brdel1 a' sum      57.5      0.0      0
*
*clivar      a0      coeff      variable name parameter no.
20513401      1.162      1.0      ctrlivar      120
20513402      -1.0      -1.0      ctrlivar      123
*
*clivar      name      type      factor      init      f c
20513500 'brdt-d10' sum      1.0      -1.0      0
*
*clivar      a0      coeff      variable name parameter no.
20513501      0.0      1.0      ctrlivar      121
20513502      -1.0      -1.0      ctrlivar      124
*
*clivar      name      type      factor      init      f c      max      max
20513600 'brdt-d10' function 1.0e99 0.0      0.2      1.0
*
*clivar      srch arg name      srch arg no.      table no.
20513601      ctrlivar      125      900
*
*clivar      name      type      factor      init      f c
20513700 'b del te' sum      57.5      0.0      0
*
*clivar      a0      coeff      variable name parameter no.
20513701      1.162      1.0      ctrlivar      120
20513702      -1.0      -1.0      ctrlivar      123
*
*clivar      name      type      factor      init      f c
20513800 'b del te' sum      1.0      1.0      0
*
*clivar      a0      coeff      variable name parameter no.
20513801      0.0      1.0      ctrlivar      121
20513802      -1.0      -1.0      ctrlivar      127
*
*clivar      name      type      factor      init      f c      max      max
20513900 'b del te' function 1.0e99 0.0      0.2      1.0
*
*clivar      srch arg name      srch arg no.      table no.
20513901      ctrlivar      128      900

```

```

*cttvar name type factor init f c
20514100 'c del te' sum 1.0 0.0 0
*
*cttvar #0 coeff variable name parameter no.
20514101 0.0 1.0 temp 40510000
20514102 -1.0 temp 41510000
*
*cttvar name type factor init f c
20514200 'ctavp 57' sum 1.0 0.0 0
*
*cttvar #0 coeff variable name parameter no.
20514201 -575.4 1.0 ctrivar 102
*
*cttvar name type factor init f c
20514300 'cti(-)1' lead lag 0.01075 0.0 0
*
*cttvar tau-1 tau-2 variable name parameter no.
20514301 20.0 0.0 ctrivar 142
*
*cttvar name type factor init f c
20514400 'c del s' sum 57.5 0.0 0
*
*cttvar #0 coeff variable name parameter no.
20514401 1.162 1.0 ctrivar 120
20514402 -1.0 ctrivar 143
*
*cttvar name type factor init f c
20514500 'c del d10' sum 1.0 -1.0 0
*
*cttvar #0 coeff variable name parameter no.
20514501 0.0 1.0 ctrivar 141
20514502 -1.0 ctrivar 144
*
*cttvar name type factor init f c max
20514600 'c del d10' function 1.0e99 0.0 0.2 1.0 max
*
*cttvar arch arg. name arch arg. no. table no.
20514601 ctrivar 145 900
*
*cttvar name type factor init f c
20514700 'c del s' sum 57.5 0.0 0
*
*cttvar #0 coeff variable name parameter no.
20514701 1.132 1.0 ctrivar 120
20514702 -1.0 ctrivar 143
*
*cttvar name type factor init f c
20514800 'c del d' sum 1.0 -1.0 0
*
*cttvar #0 coeff variable name parameter no.
20514801 0.0 1.0 ctrivar 141
20514802 -1.0 ctrivar 147
*
*cttvar name type factor init f c max
20514900 'c del d' function 1.0e99 0.0 0.2 1.0 max
*
*cttvar arch arg. name arch arg. no. table no.
20514901 ctrivar 148 900

```

\$the following control variables calculate the reactor / r-power delta  
 \$temp trip status. control variables 151 through 156 / r sent the  
 \$a loop, 161, 166 and 171, 176 represent the b and c loops, respectively.

```

$documentation is on pages 28-29.
*cttvar name type factor init f c min
20515000 'arop kb' sum 2.225e-3 0.0 0.1 0.0
*
*cttvar #0 coeff variable name parameter no.
20515101 -575.4 1.0 ctrivar 101
*
*cttvar name type factor init f c
20515200 'ardtavg' diffend 0.20 0.0 0
*
*cttvar divar/dt name divar/dt no.
20515201 ctrivar 101
*
*cttvar name type factor init f c min
20515300 'ardt lag' lag 1.0 0.0 0.1 0.0
*
*cttvar tau-1 variable name parameter no.
20515301 10.0 ctrivar 152
*
*cttvar name type factor init f c
20515400 'arop net' sum 57.5 57.5 0
*
*cttvar #0 coeff variable name parameter no.
20515401 1.072 -1.0 ctrivar 151
20515402 -1.0 ctrivar 153
*
*cttvar name type factor init f c
20515500 'arop t0' sum 1.0 -1.0 0
*
*cttvar #0 coeff variable name parameter no.
20515501 0.0 1.0 ctrivar 151
20515502 1.0 ctrivar 154
*
*cttvar name type factor init f c max max
20515600 'arop t0' function 1.0e99 0.0 0.2 1.0
*
*cttvar arch arg. name arch arg. no. table no.
20515601 ctrivar 155 900
$the following control variables - 157 through 159 - calculate the  

  turbine over power trip status. the b and c loops use 167-169 and  

  177-179, respectively. Documentation is on page 30.
*cttvar name type factor init f c
20515700 'atop del' sum 17.5 57.5 0
*
*cttvar #0 coeff variable name parameter no.
20515701 1.042 1.0 ctrivar 151
20515702 -1.0 ctrivar 153
*
*cttvar name type factor init f c
20515800 'atop t0' sum 1.0 1.0 0
*
*cttvar #0 coeff variable name parameter no.
20515801 0.0 1.0 ctrivar 151
20515802 -1.0 ctrivar 157
*
*cttvar name type factor init f c max max
20515900 'atop t0' function 1.0e99 0.0 0.2 1.0
*
*cttvar arch arg. name arch arg. no. table no.
20515901 ctrivar 158 900

```

```

*clivar name type factor init f c min
20516100 'brop 4b' sum 2.235e-2 0.0 0 1 0.0
*
*clivar a0 coeff variable name parameter no.
20516101 -575.4 1.0 ctrlivar 102
*
*clivar name type factor init f c
20516200 'brdtavg' diffrend 0.20 0.0 0
*
*clivar d(ivar)/dt name d(ivar)/dt no.
20516201 ctrlivar 102
*
*clivar name type factor init f c min
20516300 'brdt lag' lag 1.0 0.0 0 1 0.0
*
*clivar tau-1 variable name parameter no.
20516301 10.0 ctrlivar 102
*
*clivar name type factor init f c
20516400 'brop set' sum 57.5 57.5 0
*
*clivar a0 coeff variable name parameter no.
20516401 1.072 -1.0 ctrlivar 161
20516402 -1.0 ctrlivar 162
*
*clivar name type factor init f c
20516500 'brop 10' sum 1.0 -1.0 0
*
*clivar a0 coeff variable name parameter no.
20516501 0.0 1.0 ctrlivar 121
20516502 -1.0 ctrlivar 120
*
*clivar name type factor init f c max
20516600 'brop 10' function 1.0e99 0.0 0 2 1.0
*
*clivar arch arg. name arch arg. no. table no.
20516601 ctrlivar 165 900
*
*clivar name type factor init f c
20516700 'btop set' sum 57.5 57.5 0
*
*clivar a0 coeff variable name parameter no.
20516701 1.042 -1.0 ctrlivar 161
20516702 -1.0 ctrlivar 162
*
*clivar name type factor init f c
20516800 'btop 10' sum 1.0 -1.0 0
*
*clivar a0 coeff variable name parameter no.
20516801 0.0 1.0 ctrlivar 121
20516802 -1.0 ctrlivar 167
*
*clivar name type factor init f c max max
20516900 'btop 10' function 1.0e99 0.0 0 2 1.0
*
*clivar arch arg. name arch arg. no. table no.
20516901 ctrlivar 165 900
*
*clivar name type factor init f c min
20517100 'crop 4b' sum 2.235e-3 0.0 0 1 0.0
*
*clivar a0 coeff variable name parameter no.
20517101 -575.4 1.0 ctrlivar 102

```

```

*
*clivar name type factor init f c
20517200 'crdtavg' diffrend 0.20 0.0 0
*
*clivar d(ivar)/dt name d(ivar)/dt no.
20517201 ctrlivar 102
*
*clivar name type factor init f c min
20517300 'crdt lag' lag 1.0 0.0 0 1 0.0
*
*clivar tau-1 variable name parameter no.
20517301 10.0 ctrlivar 122
*
*clivar name type factor init f c
20517400 'crop set' sum 57.5 57.5 0
*
*clivar a0 coeff variable name parameter no.
20517401 1.072 -1.0 ctrlivar 171
20517402 -1.0 ctrlivar 172
*
*clivar name type factor init f c
20517500 'crop 10' sum 1.0 -1.0 0
*
*clivar a0 coeff variable name parameter no.
20517501 0.0 1.0 ctrlivar 141
20517502 -1.0 ctrlivar 174
*
*clivar name type factor init f c max max
20517600 'crop 10' function 1.0e99 0.0 0 2 1.0
*
*clivar arch arg. name arch arg. no. table no.
20517601 ctrlivar 175 900
*
*clivar name type factor init f c
20517700 'ctop set' sum 57.5 57.5 0
*
*clivar a0 coeff variable name parameter no.
20517701 1.042 -1.0 ctrlivar 171
20517702 -1.0 ctrlivar 172
*
*clivar name type factor init f c
20517800 'ctop 10' sum 1.0 -1.0 0
*
*clivar a0 coeff variable name parameter no.
20517801 0.0 1.0 ctrlivar 141
20517802 -1.0 ctrlivar 172
*
*clivar name type factor init f c max max
20517900 'ctop 10' function 1.0e99 0.0 0 2 1.0
*
*clivar arch arg. name arch arg. no. table no.
20517901 ctrlivar 175 900
*
The following control variables calculate the 2/3 reactor and turbine
super-temperature and over-power values, respectively. Documentation
is on pages 21-30.
*
*clivar name type factor init f c
20518000 'rdelt 2/' sum 1.0 0.0 0
*
*clivar a0 coeff variable name parameter no.
20518001 0 1.0 ctrlivar 126
20518002 1.0 ctrlivar 128
20518003 1.0 ctrlivar 140

```

```

*-----*
*ctrlvr name type factor init f c
20518100 'del 1/2' sum 1.0 0.0 0
*
*ctrlvr ad coeff variable name parameter no.
20518101 0.0 1.0 ctrlvr 120
20518102 1.0 ctrlvr 120
20518103 1.0 ctrlvr 120
20518104 1.0 ctrlvr 120
*
*ctrlvr name type factor init f c
20518200 'top 2/3' sum 1.0 0.0 0
*
*ctrlvr ad coeff variable name parameter no.
20518201 0.0 1.0 ctrlvr 120
20518202 1.0 ctrlvr 120
20518203 1.0 ctrlvr 120
20518204 1.0 ctrlvr 120
*
*ctrlvr name type factor init f c
20518300 'top 2/3' sum 1.0 0.0 0
*
*ctrlvr ad coeff variable name parameter no.
20518301 0.0 1.0 ctrlvr 120
20518302 1.0 ctrlvr 120
20518303 1.0 ctrlvr 120
20518304 1.0 ctrlvr 120
*
*the following control variables calculate the low rc flow status.
*documentation is on pages 23-26a.
*-----*
*ctrlvr name type factor init f c
20519000 'a del wd' sum 1.0 -841.67 0
*
*ctrlvr ad coeff variable name parameter no.
20519001 8510.184 -2.2046 ctrlvr 204010000
*
*ctrlvr name type factor init f c
20519100 'b del wd' sum 1.0 -841.67 0
*
*ctrlvr ad coeff variable name parameter no.
20519101 8510.184 -2.2046 ctrlvr 204010000
*
*ctrlvr name type factor init f c
20519200 'c del wd' sum 1.0 -841.67 0
*
*ctrlvr ad coeff variable name parameter no.
20519201 8510.184 -2.2046 ctrlvr 404010000
*
*ctrlvr name type factor init f c max max
20519300 'a rc err' function 1.0e99 0.0 0.2 1.0
*
*ctrlvr brch arg name brch arg. no. table no.
20519301 ctrlvr 180 900
*
*ctrlvr name type factor init f c max max
20519400 'b rc err' function 1.0e99 0.0 0.2 1.0
*
*ctrlvr brch arg name brch arg. no. table no.
20519401 ctrlvr 181 900
*
*ctrlvr name type factor init f c max max
20519500 'c rc err' function 1.0e99 0.0 0.2 1.0
*
*ctrlvr brch arg name brch arg. no. table no.
20519501 ctrlvr 182 900

```

```

*-----*
*ctrlvr name type factor init f c
20519600 'rc low f' sum 1.0 0.0 0
*
*ctrlvr ad coeff variable name parameter no.
20519601 0.0 1.0 ctrlvr 193
20519602 1.0 ctrlvr 194
20519603 1.0 ctrlvr 195
*
*ctrlvr name type factor init f c
20519700 '8 loops' function 1.0 1.0 0
*
*ctrlvr brch arg name brch arg. no. table no.
20519701 ctrlvr 190 192
*
*the following control variables - 200 through 206 - represent the
*pressurizer level control system. documentation is on pages 26-45.
*-----*
*ctrlvr name type factor init f c min max
20520000 'par sp 1' sum 1.0 0.532 0.3 0.222 0.533
*
*ctrlvr ad coeff variable name parameter no.
20520001 -0.03230 1.1433e-2 ctrlvr 104
*
*ctrlvr name type factor init f c
20520100 'par dp 1' sum 1.0 0.227118 1.3 0.0 1.0
*
*ctrlvr ad coeff variable name parameter no.
20520101 0.20759 2.2184e-5 p 341010000
20520102 -1.16443e-5 p 340010000
20520103 -1.03406e-5 p 341010000
*
*ctrlvr name type factor init f c min max
20520200 'par leve' lag 1.0 0.227118 1.3 0.0 1.0
*
*ctrlvr tau-1 variable name parameter no.
20520201 0.796 ctrlvr 201
*
*ctrlvr name type factor init f c
20520300 'par lsp' sum 1.0 0.0 0
*
*ctrlvr ad coeff variable name parameter no.
20520301 0.0 1.0 ctrlvr 200
20520302 1.0 ctrlvr 202
*
*ctrlvr name type factor init f c
20520400 'cvcs d r' prop-int 10.0 0.0 0.3 -0.80040 1.0
*
*ctrlvr prop gain int. gain variable name parameter no.
20520401 1.0 5.5557e-3 ctrlvr 203
*
*ctrlvr name type factor init f c
20520500 'bias off' trip-hst 1.0 1.0 0
*
*ctrlvr trip no.
20520501 658
*
*ctrlvr name type factor init f c min max
20520600 'cvcs inj' sum 1.0 54.0 0.3 0.0 154.0
*
*ctrlvr ad coeff variable name parameter no.
20520601 54.0 37.0 ctrlvr 204
*
*ctrlvr name type factor init f c min max

```



```

20520700 'net cvct' sum 1.0 0.0 0.0 -54.0 164.0
*ctrlvar name type factor init f c
20520701 a0 coeff 1.0 variable name parameter no.
20520702 0.0 1.0 ctrlivar 205
20520703 -54.0 ctrlivar 205
*ctrlvar variable name parameter no.
20520704 y 240010000
*ctrlvar name type factor init f c
20521000 'par pres' mult 1.46037e-4 2250 0 0
*ctrlvar variable name parameter no.
20521100 y 240010000
*ctrlvar name type factor init f c
20521100 'par p-pr' sum 1.0 0.0 0
*ctrlvar a0 coeff variable name parameter no.
20521101 -2250 0 1.0 ctrlivar 210
20521102 0.0 1.0 ctrlivar 210
*ctrlvar name type factor init f c
20521200 'p comp e' prop-int 1.0 0.0 0.0 -25.0 100.0
*ctrlvar prop gain int gain variable name parameter no.
20521201 1 0 8.23255e-2 ctrlivar 211
20521202 0.0 1.0 ctrlivar 211
*ctrlvar name type factor init f c min max
20521300 'p spray' sum 1.0 0.0 0.0 0.0 1.0
*ctrlvar a0 coeff variable name parameter no.
20521301 -0.50 0.020 ctrlivar 212
20521302 0.0 1.0 ctrlivar 212
*ctrlvar name type factor init f c
20521400 'p htr tr' tripunit 1.0 0.0 0
*ctrlvar trip no.
20521401 610
*ctrlvar name type factor init f c min max
20521500 'p phtr q' sum 0.266 0.0 0.0 0.0 0.266
*ctrlvar a0 coeff variable name parameter no.
20521501 0.00 -6.68867e-02 ctrlivar 213
20521502 0.0 1.0 ctrlivar 213
*ctrlvar name type factor init f c
20521600 'p phtr q' mult 1.0 0.0 0
*ctrlvar variable name parameter no. variable name parameter no.
20521601 ctrlivar 214 ctrlivar 215
20521602 0.0 1.0 ctrlivar 214
*ctrlvar name type factor init f c
20521700 'p on-off' tripunit 0.966 0.0 0
*ctrlvar trip no.
20521701 612
*ctrlvar name type factor init f c
20521800 'p pvl op' tripunit 0.25 0.0 0
*ctrlvar trip no.
20521801 614

```

```

*ctrlvar name type factor init f c
20521900 'p pvl cl' tripunit -0.5 -0.5 0
*ctrlvar trip no.
20521901 614
*ctrlvar name type factor init f c
20522000 'p pvl d1' sum -1.0 -1.0 0
*ctrlvar a0 coeff variable name parameter no.
20522001 0.0 1.0 ctrlivar 216
20522002 1.0 ctrlivar 216
*ctrlvar name type factor init f c min max
20522100 'p pvl da' mult 1.0 0.0 0.0 -0.5 0.5
*ctrlvar variable name parameter no. variable name parameter no.
20522101 ctrlivar 201 ctrlivar 220
*ctrlvar name type factor init f c
20522200 'p pv2 up' tripunit 0.25 0.0 0
*ctrlvar trip no.
20522201 616
*ctrlvar name type factor init f c
20522300 'p pv2 cl' tripunit -0.5 -0.5 0
*ctrlvar trip no.
20522301 616
*ctrlvar name type factor init f c
20522400 'p pv2 d1' sum 1.0 -1.0 0
*ctrlvar a0 coeff variable name parameter no.
20522401 0.0 1.0 ctrlivar 222
20522402 1.0 ctrlivar 222
*ctrlvar name type factor init f c min max
20522500 'p pv2 da' mult 1.0 0.0 0.0 0.5 0.5
*ctrlvar variable name parameter no. variable name parameter no.
20522501 ctrlivar 201 ctrlivar 224
*ctrlvar name type factor init f c min max
20522600 'pov 1 a' sum 1.0 0.0 0.0 0.0 0.5
*ctrlvar a0 coeff variable name parameter no.
20522702 0.0 1.0 ctrlivar 225
20522703 1.0 ctrlivar 225
*ctrlvar name type factor init f c min max
20522700 'pov 2 a' sum 1.0 0.0 0.0 0.0 0.5
*ctrlvar a0 coeff variable name parameter no.
20522702 0.0 1.0 ctrlivar 226
20522703 1.0 ctrlivar 226
*ctrlvar name type factor init f c min max
20522800 'p pov a' sum 1.0 0.0 0.0 0.0 1.0
*ctrlvar a0 coeff variable name parameter no.
20522802 0.0 1.0 ctrlivar 226

```

The following control variable closes the feedback loop and is \*  
 sequentially upon actuation of dist. see also control variables \*  
 528, 628, and 728.

```
*ctrlvar name type factor init f c
20549500 'dist on' tripoint 1.0 0.0 0
*
*ctrlvar trij no.
20549901 008
*
```

The following control variables - 500 through 528 - represent the 500  
 level control system. control variables 501 through 528 and 701  
 through 728 represent the b and c gene stores, respectively.  
 Documentation is on pages 53-71

```
*ctrlvar name type factor init f c
20550000 'a r f la' sum 1.0 0.0 0
*
```

```
*ctrlvar a0 coeff variable name parameter no.
20550001 0.0 1.45037e-4 b 270010000
20550002 2.04546e-4 rhb 270010000
```

```
*ctrlvar name type factor init f c
20550100 'a wr lap' sum 1.0 0.0 0
*
```

```
*ctrlvar a0 coeff variable name parameter no.
20550101 0.0 1.45037e-4 b 262040000
20550102 2.75486e-4 rhb 262040000
```

```
*ctrlvar name type factor init f c min max
20550200 'a r r niv' sum 1.0 0.000 0.0 0.0 1.0
*
```

```
*ctrlvar a0 coeff variable name parameter no.
20550201 -3.80776e-2 7.29735e-2 ctrlvar 501
20550202 -7.29735e-2 ctrlvar 500
```

```
*ctrlvar name type factor init f c
20550300 'a wr lev' sum 1.0 0.0 0
*
```

```
*ctrlvar variable name parameter no.
20550301 ctrlvar 502
```

```
*ctrlvar name type factor init f c
20550500 'a p r r i' sum 1.0 0.0 0
*
```

```
*ctrlvar a0 coeff variable name parameter no.
20550501 0.0 1.45037e-4 b 250010000
20550502 -4.89176e-5 rhb 250010000
```

```
*ctrlvar name type factor init f c min max
20550600 'a nr n i' sum 1.0 0.0 0.0 0.0 1.0
*
```

```
*ctrlvar a0 coeff variable name parameter no.
20550601 -3.10776e-2 0.26179 ctrlvar 505
20550602 -0.26179 ctrlvar 500
```

```
*ctrlvar name type factor init f c
20550700 'a nr lev' sum 1.0 0.0 0
*
```

```
*ctrlvar variable name parameter no.
20550701 ctrlvar 506
```

```
*ctrlvar name type factor init f c
20550800 'a nr lus' lag 1.0 0.52 0
*
```

```
*ctrlvar tau-1 variable name parameter no.
20550801 1.0 ctrlvar 506
```

```
*ctrlvar name type factor init f c min max
20551000 'sp niv' sum 1.0 0.52 0.0 0.0 0.52
*
```

```
*ctrlvar a0 coeff variable name parameter no.
20551001 0.37224 1.75730e-7 b 800010000
```

```
*ctrlvar name type factor init f c
20551100 'a lvl er' sum 1.0 0.0 0
*
```

```
*ctrlvar a0 coeff variable name parameter no.
20551101 0.0 1.0 ctrlvar 510
20551102 -1.0 ctrlvar 500
```

```
*ctrlvar name type factor init f c
20551200 'a lvl pi' prop-int 0.3 0.0 0.0 0.0 2.0
*
```

```
*ctrlvar prop gain int gain variable name parameter no.
20551201 1.0 5.55555e-4 ctrlvar 511
```

```
*ctrlvar name type factor init f c
20551300 'a lvl er' sum 1.0 0.0 0
*
```

```
*ctrlvar a0 coeff variable name parameter no.
20551301 0.0 1.0 ctrlvar 512
20551302 1.08414e-2 wflow 551000000
20551303 -1.08414e-3 wflow 551000000
```

```
*ctrlvar name type factor init f c
20551400 'a fuv dm' prop-int 1.0 0.0 0.0 4.0 5.0
*
```

```
*ctrlvar prop gain int gain variable name parameter no.
20551401 1.0 0.0 ctrlvar 513
```

```
*ctrlvar name type factor init f c
20551500 'wfl gsm' null 244.070 1500.0 0
*
```

```
*ctrlvar variable name parameter no.
20551501 wfl gsm 800000000
```

```
*ctrlvar name type factor init f c
20551600 'wfl2 gsm' null 244.070 1500.0 0
*
```

```
*ctrlvar variable name parameter no.
20551601 wfl2 gsm 800000000
```

```
*ctrlvar name type factor init f c
20551700 'hw flow' sum 2.2085 0.0 0
*
```

```
*ctrlvar a0 coeff variable name parameter no.
20551701 0.0 1.0 wflow 804000000
20551702 1.0 wflow 808000000
20551703 1.0 wflow 808000000
20551704 1.0 wflow 808000000
20551705 1.0 wflow 824020000
20551706 1.0 wflow 551000000
20551707 1.0 wflow 830000000
```

```

20551708      -1.0      mflow      730000000
20551709      -1.0      mflow      640000000
20551710      -1.0      mflow      640000000
20551711      -1.0      mflow      740000000
*-----*
*cliver      name      type      factor      init      f c      min
20551800 'fw wate' integral 1.0 252056.13 0 1 0.0
*
*cliver      integrand name      integrand no.
20551901      cliver      517
*-----*
*cliver      name      type      factor      init      f c
20551900 'fw stat' tripunit 1.0 0.0 0
*
*cliver      trip no.
20551901      531
*-----*
*cliver      name      type      factor      init      f c
20552000 'fw viv 1' tripunit 1.0 0.0 0
*
*cliver      trip no.
20552001      531
*-----*
*cliver      name      type      factor      init      f c
20552100 'a old fw' mult 1.0 0.0 0
*
*cliver      variable name      parameter no.      variable name      parameter no.
20552101      cliver      520      cliver      524
*-----*
*cliver      name      type      factor      init      f c      min      max
20552200 'a adj de' sum 1.0 0.0 0 3 -1.0 1.0
*
*cliver      a0      coeff      variable name      parameter no.
20552201      0.0      1.0      cliver      514
20552202      -10.0      cliver      520
*-----*
*cliver      name      type      factor      init      f c
20552300 'a fw ga' mult 0.10 0.0 0
*
*cliver      variable name      parameter no.      variable name      parameter no.
20552301      cliver      501      cliver      522
*-----*
*cliver      name      type      factor      init      f c      min      max
20552400 'a fw ar' sum 1.0 0.706511 0 3 0.0 1.0
*
*cliver      a0      coeff      variable name      parameter no.
20552401      0.0      0.706510      cliver      519
20552402      1.00      cliver      521
20552403      1.00      cliver      523
*-----*
*cliver      name      type      factor      init      f c
20552500 'hotstand' tripunit 1.0 0.0 0
*
*cliver      trip no.
20552501      533
*-----*
*cliver      name      type      factor      init      f c
20552600 'a fw fi' tripunit 0.01 0.0 0 0
*
*cliver      trip no.
20552601      537
*-----*
*cliver      name      type      factor      init      f c

```

```

20552700 'a fw da' mult 1.0 0.0 0 0
*
*cliver      variable name      parameter no.      variable name      parameter no.
20552701      cliver      523      cliver      525
20552702      cliver      526
*-----*
*cliver      name      type      factor      init      f c      min      max
20552800 'a fw ar' sum 1.0 0.0 0 3 0.0 1.0
*
*cliver      a0      coeff      variable name      parameter no.
20552801      0.0      1.0      cliver      527
20552802      -100.0      cliver      490
*-----*
*cliver      name      type      factor      init      f c      min      max
20552900 'a til fw' sum 1.0 0.52 0 3 0.0 1.0
*
*cliver      a0      coeff      variable name      parameter no.
20552901      0.0      1.0      cliver      524
20552902      1.0      cliver      528
*-----*
$main feedwater pump bypass control logic
*-----*
*cliver      name      type      factor      init      f c
20554000 'a rc ope' tripunit 1.0 0.0 0 0
*
*cliver      trip number
20554001      722
*
*cliver      name      type      factor      init      f c
20554100 'b rc ope' tripunit 1.0 0.0 0 0
*
*cliver      trip number
20554101      726
*-----*
$calculate the total flow through both recirculation lines
*-----*
*cliver      name      type      factor      init      f c
20554200 't rc ope' sum 0.5 0.0 0
*
*cliver      a0      coeff      variable name      parameter no.
20554301      0.0      1.0      cliver      540
20554302      1.0      cliver      541
*-----*
*cliver      name      type      factor      init      f c
20554300 'recirc a' sur 1.45237e-4 0 0 1
*
*cliver      a0      coeff      variable name      parameter no.
20554301      0.0      1.0      p      867010000
20554302      -1.0      p      822010000
*-----*
*cliver      name      type      factor      init      f c      min
20554400 'rc div' div 15.0178 0.0 1 1 0.0
*
*cliver      divisor name      divisor no.      dividend name      dividend no.
20554401      rto      867010000      cliver      543
*-----*
*cliver      name      type      factor      init      f c      min
20554500 'rc vel' stdfnctn 7.81896 0.0 0 1 0.0
*
*cliver      function      variable name      parameter no.
20554501      r2      cliver      544
*-----*
*cliver      name      type      factor      init      f c

```

```

20554800 'i rc w1' mult 1.0 0.0 0
*
*clivar variable name parameter no. variable name parameter no.
20554801 ctrlivar 545 ctrlivar 545
*.....*
$steep generator a safety valve control system
*.....*
$convert pressure in volume 560 to psig
*.....*
*clivar name type factor init f c
20554900 'p conv' sum 1.0 0.0 1
*
*clivar a0 coeff variable name parameter no.
20554901 -14.7 1.45038e-04 p 56010000
*.....*
$check if on upper hysteresis curve or lower curve
*.....*
*clivar name type factor init f c
20554900 'sup of c' tripunit 1.0 0.0 0
*
*clivar trip no.
20554901 542
*.....*
$calculate the difference between the upper curve and the lower curve
*.....*
*clivar name type factor init f c
20554900 'area dif' function 1.0 0.0 1
*
*clivar arch arg. name arch arg. no. table no.
20554901 ctrlivar 551 500
*.....*
$multiply the difference by the tripunit to determine use of upper or
lower curve
*.....*
*clivar name type factor init f c
20554900 'up or de' mult 1.0 0.0 1
*
*clivar variable name parameter no. variable name parameter no.
20554901 ctrlivar 552 ctrlivar 552
*.....*
$calculate the valve area used on the lower curve with corresponding p
*.....*
*clivar name type factor init f c
20554900 'low area' function 1.0 0.0 1
*
*clivar arch arg. name arch arg. no. table no.
20554901 ctrlivar 551 501
*.....*
$calculate the normalized valve area for safety valve a
*.....*
*clivar name type factor init f c min max
20554900 'a norm a' sum 1.0 0.0 1.2 0.0 1.0
*
*clivar a0 coeff variable name parameter no.
20554901 0.0 1.0 ctrlivar 554
20554902 1.0 ctrlivar 555
*.....*
$loop a primary to secondary heat transfer
*.....*
*clivar name type factor init f c
20557000 'aq pri/s' sum 1.0 0.0 0 0
*
*clivar a0 coeff variable name parameter no.

```

```

20557001 0.0 1.0e-6 q 26601001
20557002 1.0e-6 q 266020000
20557003 1.0e-6 q 266030000
20557004 1.0e-6 q 26604
*.....*
*clivar name type factor init f c
20560000 'b ref la' sum 1.0 0.0 0
*
*clivar a0 coeff variable name parameter no.
20560001 0.0 1.45037e-4 p 27010000
20560002 8.04345e-4 rho 178010000
*.....*
*clivar name type factor init f c
20560100 'b wr tap' sum 1.0 0.0 0
*
*clivar a0 coeff variable name parameter no.
20560101 0.0 1.45037e-4 p 262040000
20560102 8.70548e-4 rho 262040000
*.....*
*clivar name type factor init f c min max
20560700 'b wr niv' sum 1.0 0.950 0.9 0.0 1.0
*
*clivar a0 coeff variable name parameter no.
20560701 -3.60776e-2 7.29735e-2 ctrlivar 601
20560702 -7.29735e-2 ctrlivar 600
*.....*
*clivar name type factor init f c
20560700 'b wr lev' mult 143.0 0.0 0
*
*clivar variable name parameter no.
20560801 ctrlivar 502
*.....*
*clivar name type factor init f c
20560800 'b p nr l' sum 1.0 0.0 0
*
*clivar a0 coeff variable name parameter no.
20560801 0.0 1.45037e-4 p 258010000
20560802 -4.89179e-5 rho 258010000
*.....*
*clivar name type factor init f c min max
20560800 'b nr l' sum 1.0 .52 0.3 0.0 1.0
*
*clivar a0 coeff variable name parameter no.
20560801 -3.20776e-2 0.26179 ctrlivar 605
20560802 0.26179 ctrlivar 600
*.....*
*clivar name type factor init f c
20560700 'b nr lev' mult 143.0 74.30 0
*
*clivar variable name parameter no.
20560701 ctrlivar 600
*.....*
*clivar name type factor init f c
20560800 '% c lev' lag 1.0 0.52 0
*
*clivar tau-1 variable name parameter no.
20560801 0.0 ctrlivar 506
*.....*
*clivar name type factor init f c
20561100 'b lvl er' sum 1.0 0.0 0
*
*clivar a0 coeff variable name parameter no.
20561101 0.0 1.0 ctrlivar 610

```





```

20566002 1.0 ctrlivar 655
loop b primary to secondary heat transfer
*ctrlvar name type factor init f c
20567000 'bq pri/s' sum 1.0 0.0 0.0
*
*ctrlvar a0 coeff variable name parameter no.
20567001 0.0 1.0e-6 q 360010000
20567002 1.0e-6 q 360020000
20567003 1.0e-6 q 360030000
20567004 1.0e-6 q 360040000
*
*ctrlvar name type factor init f c
20570000 'c ref la' sum 1.0 0.0 0
*
*ctrlvar a0 coeff variable name parameter no.
20570001 0.0 1.45037e-4 p 470010000
20570002 3.04385e-4 rho 470010000
*
*ctrlvar name type factor init f c
20570100 'c wr tag' sum 1.0 0.0 0
*
*ctrlvar a0 coeff variable name parameter no.
20570101 0.0 1.45037e-4 p 462040000
20570102 0.70548e-4 rho 462040000
*
*ctrlvar name type factor init f c min max
20570200 'c wr niv' sum 1.0 0.000 0.3 0.0 1.0
*
*ctrlvar a0 coeff variable name parameter no.
20570201 -3.80778e-2 7.28725e-1 ctrlivar 701
20570202 -7.28725e-2 ctrlivar 700
*
*ctrlvar name type factor init f c
20570300 'c wr lev' mult 013.0 0.0 0
*
*ctrlvar variable name parameter no.
20570301 ctrlivar 702
*
*ctrlvar name type factor init f c
20570500 'c p nr i' sum 1.0 0.0 0
*
*ctrlvar a0 coeff variable name parameter no.
20570501 0.0 1.45037e-4 p 450010000
20570502 -4.89178e-5 rho 450010000
*
*ctrlvar name type factor init f c min max
20570600 'c nr n i' sum 1.0 0.2 0.3 0.0 1.0
*
*ctrlvar a0 coeff variable name parameter no.
20570601 -3.80778e-2 0.26179 ctrlivar 705
20570602 -0.26179 ctrlivar 700
*
*ctrlvar name type factor init f c
20570700 'c nr lev' mult 143.0 74.36 0
*
*ctrlvar variable name parameter no.
20570701 ctrlivar 706
*
*ctrlvar name type factor init f c
20570800 'c nr lus' leg 1.0 0.52 0

```

```

*
*ctrlvar tau_i variable name parameter no.
20570901 0.0 ctrlivar 700
*
*ctrlvar csm type factor init f c
20571100 'c ivl sr' sum 1.0 0.0 0
*
*ctrlvar a0 coeff variable name parameter no.
20571101 0.0 1.0 ctrlivar 610
20571102 -1.0 ctrlivar 708
*
*ctrlvar name type factor init f c
20571200 'c ivl pi' prop-int 3.3 0.0 0.3 -3.0 2.0
*
*ctrlvar prop gain int gain variable name parameter no.
20571201 1.0 5.55556e-4 ctrlivar 711
*
*ctrlvar name type factor init f c
20571300 'c tll sr' sum 1.0 0.0 0
*
*ctrlvar a0 coeff variable name parameter no.
20571301 0.0 1.0 ctrlivar 712
20571302 1.00414e-3 wflow 750000000
20571303 -1.00414e-3 wflow 250000000
*
*ctrlvar name type factor init f c
20571400 'c fuv dm' prop-int 1.0 0.0 0.3 -4.0 3.0
*
*ctrlvar prop gain int gain variable name parameter no.
20571401 1.0 0.000 ctrlivar 713
*
*ctrlvar name type factor init f c
20572100 'c pid fw' mult 1.0 0.0 0
*
*ctrlvar variable name parameter no. variable name parameter no.
20572101 ctrlivar 520 ctrlivar 714
*
*ctrlvar name type factor init f c min max
20572200 'c adj de' sum 1.0 0.0 0.3 -1.0 3.0
*
*ctrlvar a0 coeff variable name parameter no.
20572201 0.0 1.0 ctrlivar 714
20572202 -10.0 ctrlivar 520
*
*ctrlvar name type factor init f c
20572300 'c fuv de' mult 0.10 0.0 0
*
*ctrlvar variable name parameter no. variable name parameter no.
20572301 ctrlivar 601 ctrlivar 722
*
*ctrlvar name type factor init f c min max
20572400 'c fuv sr' sum 1.0 0.705393 0.3 0.0 1.0
*
*ctrlvar a0 coeff variable name parameter no.
20572401 0.0 0.705398 ctrlivar 610
20572402 1.0 ctrlivar 721
20572403 1.0 ctrlivar 723
*
*ctrlvar name type factor init f c
20572600 'c fab fj' sripunit 0.01 0.0 0.0
*
*ctrlvar srip no.
20572601 589

```

```

*ctrlvar name type factor init f c
20572700 'c Feb dg' sum 1.0 0.0 0 0
*
*ctrlvar variable name parameter no. variable name parameter no.
20572701 ctrlvar 723 ctrlvar 525
20572702 ctrlvar 726
*
*ctrlvar name type factor init f c min max
20572800 'c Feb ar' sum 1.0 0.0 0 3 0.0 1.0
*
*ctrlvar a0 coeff variable name parameter no.
20572801 0.0 1.0 ctrlvar 727
20572802 -100.0 ctrlvar 499
*
*ctrlvar name type factor init f c min max
20572900 'c tll fa' sum 1.0 0.52 0 3 0.0 1.0
*
*ctrlvar a0 coeff variable name parameter no.
20572901 0.0 1.0 ctrlvar 724
20572902 1.0 ctrlvar 728
*
the following control variables represent the motor driven afc
$control, documentation is on pages 78-80.
*
*ctrlvar name type factor init f c
20573000 'afw min' sidfnctn 1.45037e-4 900.0 0
*
*ctrlvar function
20573001 min
*ctrlvar variable name parameter no. variable name parameter no.
20573002 p 520010000 p 520010000
20573003 p 520010000
*
*ctrlvar name type factor init f c
20573100 'a lvi 15' tripunit 1.0 0.0 0
*
*ctrlvar trip no.
20573101 536
*
*ctrlvar name type factor init f c
20573200 'b lvi 15' tripunit 1.0 0.0 0
*
*ctrlvar trip no.
20573201 537
*
*ctrlvar name type factor init f c
20573300 'c lvi 15' tripunit 1.0 0.0 0
*
*ctrlvar trip no.
20573301 538
*
*ctrlvar name type factor init f c
20573400 'Mag # 15' sum 1.0 0.0 0
*
*ctrlvar a0 coeff variable name parameter no.
20573401 1.0 1.0 ctrlvar 731
20573402 1.0 1.0 ctrlvar 732
20573403 1.0 1.0 ctrlvar 733
*
Steam generator c safety valve control system

```

Convert pressure in volume 750 to psia

```

*ctrlvar name type factor init f c
20575100 'p cnvrt' sum 1.0 0.0 1
*
*ctrlvar a0 coeff variable name parameter no.
20575101 -14.7 1.45038e-04 p 750010000
*
check if on upper hysteresis curve or lower curve
*
*ctrlvar name type factor init f c
20575200 'cup of c' tripunit 1.0 0.0 0
*
*ctrlvar trip no.
20575201 644
*
calculate the difference between the upper curve and the lower curve
*
*ctrlvar name type factor init f c
20575300 'area dif' function 1.0 0.0 1
*
*ctrlvar srch arg. name srch arg. no. table no.
20575301 ctrlvar 751 500
*
multiply the difference by the tripunit to determine use of upper or
lower curve
*
*ctrlvar name type factor init f c
20575400 'up or dn' sum 1.0 0.0 1
*
*ctrlvar variable name parameter no. variable name parameter no.
20575401 ctrlvar 752 ctrlvar 753
*
calculate the valve area used on the lower curve with corresponding p
*
*ctrlvar name type factor init f c
20575500 'low area' function 1.0 0.0 1
*
*ctrlvar srch arg. name srch arg. no. table no.
20575501 ctrlvar 751 501
*
calculate the normalized valve area for safety valve c
*
*ctrlvar name type factor init f c min max
20575600 'c norm a' sum 1.0 0.0 1 3 0.0 1.0
*
*ctrlvar a0 coeff variable name parameter no.
20575601 0.0 1.0 ctrlvar 754
20575602 1.0 1.0 ctrlvar 755
*
loop c primary to secondary heat transfer
*
*ctrlvar name type factor init f c
20577000 'cg pt. ys' sum 1.0 0.0 0 0
*
*ctrlvar a0 coeff variable name parameter no.
20577001 0.0 1.0e-6 q 46010000
20577002 1.0e-6 q 46020000
20577003 1.0e-6 q 46030000
20577004 1.0e-6 q 46040000
*
total primary to secondary heat transfer
*
*ctrlvar name type factor init f c
20577100 'q total' sum 1.0 0.0 0 0

```

```

*ctrlvar      a0      coeff      variable name parameter no.
20577101      0.0      1.0      ctrlvar      570
20577102      1.0      1.0      ctrlvar      570
20577103      1.0      1.0      ctrlvar      770
*.....*
The following control variables represent the steam dump control
variables. The load rejection controller is modeled with control
variables 800 through 815 (pages 93-94). The plant trip controller
is represented with control variables 820 through 823 (pages 95-96).
The steam pressure controller is modeled with control variables 824
through 831 (pages 99-101) and the steam line pressure controller is
modeled with control variables 832 through 841 (pages 102-104). The
steam dump system controllers are the used to determine dump and purv
Sarae demands with control variables 845 through 848 (pages 105-106).
*.....*

```

```

*ctrlvar      name      type      factor      init      f c
20580000 'lrbn pre'      mult      1.45037e-4 553.0      0
*
*ctrlvar      variable name      parameter no.
20580001      0      800010000
*.....*
*ctrlvar      name      type      factor      init      f c
20580100 'ptrbn/dt'      diffrend -120.0      0.0      0
*
*ctrlvar      d(var)/dt name      d(var)/dt no.
20580101      ctrlvar      300
*.....*
*ctrlvar      name      type      factor      init      f c
20580200 'fil p/dt'      lag      1.0      0.0      0
*
*ctrlvar      tau-1      variable name      parameter no.
20580201      120.0      ctrlvar      801
*.....*
*ctrlvar      name      type      factor      init      f c
20580300 '15A lr'      tripunit 1.0      0.0      0
*
*ctrlvar      trip no.
20580301      851
*.....*
*ctrlvar      name      type      factor      init      f c
20580400 '35A lr'      tripunit 1.0      0.0      0
*
*ctrlvar      trip no.
20580401      853
*.....*
*ctrlvar      name      type      factor      init      f c
20580500 '55A lr'      tripunit 1.0      0.0      0
*
*ctrlvar      trip no.
20580501      855
*.....*
*ctrlvar      name      type      factor      init      f c
20580600 '1rc stat'      tripunit 1.0      1.0      0
*
*ctrlvar      trip no.
20580601      858
*.....*
*ctrlvar      name      type      factor      init      f c
20580700 'comp sav'      lead lag 1.0      575.4      0
*
*ctrlvar      tau-1      tau-2      variable name      parameter no.

```

```

20580701      25.0      5.0      ctrlvar      104
*.....*
*ctrlvar      name      type      factor      init      f c
20580800 '1rc 1 ar'      sum      1.0      0.0      0
*
*ctrlvar      a0      coeff      variable name      parameter no.
20580801      0.0      1.0      ctrlvar      807
20580802      -1.0      1.0      ctrlvar      110
*.....*
*ctrlvar      name      type      factor      init      f c      min      max
20580900 'lr b1 dm'      sum      1.0      0.0      0.3      0.0      0.0
*
*ctrlvar      a0      coeff      variable name      parameter no.
20580901      -0.451128      0.02258e-2      ctrlvar      808
*.....*
*ctrlvar      name      type      factor      init      f c
20581000 'lr b1 ar'      mult      1.0      0.0      0
*
*ctrlvar      variable name      parameter no.      variable name      parameter no.
20581001      ctrlvar      809      ctrlvar      808
20581002      ctrlvar      809
*.....*
*ctrlvar      name      type      factor      init      f c      min      max
20581100 'lr b2 dm'      sum      1.0      0.0      7.3      0.0      0.4
*
*ctrlvar      a0      coeff      variable name      parameter no.
20581101      -1.04719      0.08970e-2      ctrlvar      809
*.....*
*ctrlvar      name      type      factor      init      f c
20581200 'lr b2 ar'      mult      1.0      0.0      0
*
*ctrlvar      variable name      parameter no.      variable name      parameter no.
20581201      ctrlvar      804      ctrlvar      808
20581202      ctrlvar      811
*.....*
*ctrlvar      name      type      factor      init      f c      min      max
20581300 'lr bp ar'      sum      1.0      0.0      0.8      0.0      3.0
*
*ctrlvar      a0      coeff      variable name      parameter no.
20581301      0.0      1.0      ctrlvar      810
20581302      1.0      1.0      ctrlvar      812
*.....*
*ctrlvar      name      type      factor      init      f c      min      max
20581400 'lr rv dm'      sum      1.0      0.0      0.3      0.0      1.0
*
*ctrlvar      a0      coeff      variable name      parameter no.
20581401      -2.1250      0.70583e-02      ctrlvar      808
*.....*
*ctrlvar      name      type      factor      init      f c
20581500 'lr rv ar'      mult      1.0      0.0      0
*
*ctrlvar      variable name      parameter no.      variable name      parameter no.
20581501      ctrlvar      805      ctrlvar      808
20581502      ctrlvar      814
*.....*
*ctrlvar      name      type      factor      init      f c
20582000 'pic stat'      tripunit 1.0      0.0      0
*
*ctrlvar      trip no.
20582001      859
*.....*
*ctrlvar      name      type      factor      init      f c
20582100 'pic 1 ar'      sum      1.0      28.4      0
*

```

```

*clivar      a0      coeff      variable name parameter no.
20582101      543.0      1.0      cn,river      807
*
*clivar      name      type      factor      init      f c      min      max
20582200 'pic dnd'      null      2.33333e-2 0.0      0.0      0.0      1.0
*
*clivar      variable name parameter no.
20582201      cn,river      821
*
*clivar      name      type      factor      init      f c
20582300 'pic area'      null      1.0      0.0      0
*
*clivar      variable name parameter no.      variable name parameter no.
20582301      cn,river      820      cn,river      822
*
*clivar      name      type      factor      init      f c
20582400 'pic p vs'      lag      1.45037e-4 741.95 0
*
*clivar      tau-1      variable name parameter no.
20582401      1.0      p      800010000
*
*clivar      name      type      factor      init      f c
20582500 'apc sta' tripunit      1.0      0.0      0
*
*clivar      trip no.
20582501      857
*
*clivar      name      type      factor      init      f c
20582500 'p-hdr er'      sum      1.0      0.0      0
*
*clivar      a0      coeff      variable name parameter no.
20582601      -1020.2      1.0      cn,river      824
*
*clivar      name      type      factor      init      f c      min      max
20582700 'ap bp dm' prop-int      0.005      0.0      0.0      0.0      1.0
*
*clivar      prop gain      int gain      variable name parameter no.
20582701      1.0      5.55556e-3      cn,river      826
*
*clivar      name      type      factor      init      f c
20582800 'avgp543' tripunit      1.0      1.0      0
*
*clivar      trip no.
20582801      504
*
*clivar      name      type      factor      init      f c
20582900 'ap max a'      sum      1.0      1.0      0
*
*clivar      a0      coeff      variable name parameter no.
20582901      1.0      -0.4      cn,river      828
*
*clivar      name      type      factor      init      f c
20583000 'ap bp li' stdfncn      1.0      1.0      0
*
*clivar      function
20583001      gin
*
*clivar      variable name parameter no.      variable name parameter no.
20583002      cn,river      827      cn,river      829
*
*clivar      name      type      factor      init      f c
20583100 'ap bp er'      mult      1.0      0.0      0
*
*clivar      variable name parameter no.      variable name parameter no.

```

```

20583101      cn,river      825      cn,river      830
*
*clivar      name      type      factor      init      f c
20583200 'apc sta' tripunit      1.0      1.0      0
*
*clivar      trip no.
20583201      -605
*
*clivar      name      type      factor      init      f c
20583300 'a p-in a'      sum      1.0      0.0      0
*
*clivar      a0      coeff      variable name parameter no.
20583301      -1050.0      1.45037e-4      p      850010000
*
*clivar      name      type      factor      init      f c      min      max
20583400 'sla rv d' prop-int      0.02      0.0      0.0      0.0      1.0
*
*clivar      prop gain      int gain      variable name parameter no.
20583401      1.0      5.55556e-3      cn,river      833
*
*clivar      name      type      factor      init      f c
20583500 'sla rv a'      mult      1.0      0.0      0
*
*clivar      variable name parameter no.      variable name parameter no.
20583501      cn,river      834
*
*clivar      name      type      factor      init      f c
20583600 'b p-in a'      sum      1.0      0.0      0
*
*clivar      a0      coeff      variable name parameter no.
20583601      -1050.0      1.45037e-4      p      850010000
*
*clivar      name      type      factor      init      f c      min      max
20583700 'slb rv d' prop-int      0.02      0.0      0.0      0.0      1.0
*
*clivar      prop gain      int gain      variable name parameter no.
20583701      1.0      5.55556e-3      cn,river      836
*
*clivar      name      type      factor      init      f c
20583800 'slb rv a'      mult      1.0      0.0      0
*
*clivar      variable name parameter no.      variable name parameter no.
20583801      cn,river      837
*
*clivar      name      type      factor      init      f c
20583900 'c p-in a'      sum      1.0      0.0      0
*
*clivar      a0      coeff      variable name parameter no.
20583901      -1050.0      1.45037e-4      p      750010000
*
*clivar      name      type      factor      init      f c      min      max
20584000 'sic rv d' prop-int      0.02      0.0      0.0      0.0      1.0
*
*clivar      prop gain      int gain      variable name parameter no.
20584001      1.0      5.55556e-3      cn,river      839
*
*clivar      name      type      factor      init      f c
20584100 'sic rv a'      mult      1.0      0.0      0
*
*clivar      variable name parameter no.      variable name parameter no.
20584101      cn,river      840
*
*clivar      name      type      factor      init      f c

```

```

2058400 'avgp543' tripunit 1.0 1.0 0
*
*ctivar trip no.
2058401 504
*
*ctivar name type factor init f c
2058400 'cond5' g' tripunit 1.0 1.0 0
*
*ctivar trip no.
2058401 504
*
*ctivar name type factor init f c
20584700 'max lave' stdfnctn 1.0 0.0 0
*
*ctivar function
20584701 max
*ctivar variable name parameter no. variable name parameter no.
20584702 ctrlivar 813 ctrlivar 823
*
*ctivar name type factor init f c
20584800 'i overri' null 1.0 0.0 0
*
*ctivar variable name parameter no. variable name parameter no.
20584901 ctrlivar 845 ctrlivar 847
*
*ctivar name type factor init f c
20584900 'sdc bp d' stdfnctn 1.0 0.0 0
*
*ctivar function
20584901 max
*ctivar variable name parameter no. variable name parameter no.
20584902 ctrlivar 831 ctrlivar 848
*
*ctivar name type factor init f c
20585000 'sdc bp g' null 1.0 0.0 0
*
*ctivar variable name parameter no. variable name parameter no.
20585001 ctrlivar 846 ctrlivar 849
*
*ctivar name type factor init f c
20585100 'a prv de' stdfnctn 1.0 0.0 0
*
*ctivar function
20585101 max
*ctivar variable name parameter no. variable name parameter no.
20585102 ctrlivar 815 ctrlivar 825
*
*ctivar name type factor init f c
20585200 'a prv ar' null 1.0 0.0 0
*
*ctivar variable name parameter no. variable name parameter no.
20585201 ctrlivar 851
*
*ctivar name type factor init f c
20585300 'b prv de' stdfnctn 1.0 0.0 0
*
*ctivar function
20585301 max
*ctivar variable name parameter no. variable name parameter no.
20585302 ctrlivar 815 ctrlivar 838
*
*ctivar name type factor init f c
20585400 'b prv ar' null 1.0 0.0 0

```

```

*
*ctivar variable name parameter no. variable name parameter no.
20585401 ctrlivar 853
*
*ctivar name type factor init f c
20585500 'c prv de' stdfnctn 1.0 0.0 0
*
*ctivar function
20585501 max
*ctivar variable name parameter no. variable name parameter no.
20585502 ctrlivar 815 ctrlivar 841
*
*ctivar name type factor init f c
20585600 'c prv ar' null 1.0 0.0 0
*
*ctivar variable name parameter no. variable name parameter no.
20585601 ctrlivar 855
*
$
$ control system for condensate system
$
$heaters 1,2,3,4,5, and 6 controller to simulate steam flow through
$the shell side of the heaters and thus the Q transferred. if the
$ turbine stop valves are open the heaters provide heat to the feedwater
$ if the valves are closed, only sensible heat is transferred to the
$ feedwater. the heat source is adjusted during steady state
$ initialization to achieve the desired feedwater temperature.
$
*ctivar name type factor init f c
20586700 'tr trip' tripunit 1.0 1.0 0 0
*
*ctivar trip no.
20586701 699
*
*ctivar name type factor init f c min max
20586800 'fw h l e' sum 2 20500e-4 0.0025 0
*
*ctivar a0 coeff variable name parameter no.
20586801 0.170 -1.0 tempf 879010000
*
*ctivar name type factor init f c min max
20586900 'fw h r d' sum 1.0 0.975073 0
*
*ctivar a0 coeff variable name parameter no.
20586901 0.0 1.0 ctrlivar 868
20586902 1.0 ctrlivar 869
*
*ctivar name type factor init f c min max
20587000 'fw h r d' null 1.0 0.975078 0.3 0.0 1.10
*
*ctivar variable name parameter no. variable name parameter no.
20587001 ctrlivar 867 ctrlivar 869
*
$the following control variables represent the mslv closure logic.
$documentation is on pages 110-115.
*ctivar name type factor init f c min max
20590000 'sp atm f' sum 1.0 1.1 0.3 0.4 1.1
*
*ctivar a0 coeff variable name parameter no.
20590001 0.225 0.875 ctrlivar 100

```



```

*cttivar name type factor init f c
20590100 'a sta fl' mult 2.35742e-3 1.0 0
*
*cttivar variable name parameter no.
20590101 wflow 855000000
*
*cttivar name type factor init f c
20590200 'b sta fl' mult 2.35742e-3 1.0 0
*
*cttivar variable name parameter no.
20590201 wflow 855000000
*
*cttivar name type factor init f c
20590300 'c sta fl' mult 2.35742e-3 1.0 0
*
*cttivar variable name parameter no.
20590301 wflow 755000000
*
*cttivar name type factor init f c
20590400 'a wsf tr' tripunit 1.0 0.0 0
*
*cttivar trip no.
20590401 580
*
*cttivar name type factor init f c
20590500 'b wsf tr' tripunit 1.0 0.0 0
*
*cttivar trip no.
20590501 581
*
*cttivar name type factor init f c
20590600 'c wsf tr' tripunit 1.0 0.0 0
*
*cttivar trip no.
20590601 582
*
*cttivar name type factor init f c
20590700 'a wsf tr' sum 1.0 0.0 0
*
*cttivar a0 coeff variable name parameter no.
20590701 0.0 1.0 cntrivar 904
20590702 1.0 cntrivar 905
20590703 1.0 cntrivar 908
*
*cttivar name type factor init f c
20590800 'a wsf tr' tripunit 1.0 0.0 0
*
*cttivar trip no.
20590801 584
*
*cttivar name type factor init f c
20590900 'b wsf tr' tripunit 1.0 0.0 0
*
*cttivar trip no.
20590901 585
*
*cttivar name type factor init f c
20591000 'c wsf tr' tripunit 1.0 0.0 0
*
*cttivar trip no.
20591001 586

```

```

*cttivar name type factor init f c
20591100 'a wsf tr' sum 1.0 0.0 0
*
*cttivar a0 coeff variable name parameter no.
20591101 0.0 1.0 cntrivar 908
20591102 1.0 cntrivar 909
20591103 1.0 cntrivar 910
*
$the following control variables model the closure of the turbine stop
$valves and the turbine governor valves. documentation is on pages
$119-125.
-----
*cttivar name type factor init f c
20591500 'trn tr' tripunit 1.0 0.0 0
*
*cttivar trip no.
20591501 674
*
*cttivar name type factor init f c
20591600 'trn da' mult 1.0 0 0
*
*cttivar variable name parameter no. variable name parameter no.
20591601 cntrivar 901 cntrivar 915
20591602 cntrivar 926
*
*cttivar name type factor init f c
20591700 'tbn sp' tripunit 0.05 0.0 0
*
*cttivar trip no.
20591701 679
*
*cttivar name type factor init f c max max
20591800 'tbn sp d' sum 1.0 1.0 0 2 1.0
*
*cttivar a0 coeff variable name parameter no.
20591801 0.0 1.0 cntrivar 918
20591802 -1.0 cntrivar 917
*
*cttivar name type factor init f c
20591900 'tbn stat' tripunit 1.0 0.0 0
*
*cttivar trip no.
20591901 -674
*
*cttivar name type factor init f c min
20592000 'tbn vlv' mult 1.0 1.0 0 1 0.0
*
*cttivar variable name parameter no. variable name parameter no.
20592001 cntrivar 916 cntrivar 919
*
*cttivar name type factor init f c
20592100 'tbn vlv' tripunit 2.3223e-2 0.0 0
*
*cttivar trip no.
20592101 -578
*
*cttivar name type factor init f c
20592200 'tbn da' mult 1.0 0.0 0
*
*cttivar variable name parameter no. variable name parameter no.
20592201 cntrivar 901 cntrivar 919
20592202 cntrivar 921

```

```

*ctrlvar name type factor init f c min
20592300 'i vlv dm' sum 1.0 1.0 0.1 0.0
*
*ctrlvar #0 coeff variable name parameter no.
20592301 0.0 1.0 ctrlivar 824
20592302 -1.0 ctrlivar 825
20592303 -1.0 ctrlivar 822
$.....$
*ctrlvar name type factor init f c min max
20592400 'i vlv ar' stiffnctn 1.0 1.0 0.3 0.0 1.0
*
*ctrlvar function
20592401
*ctrlvar variable name parameter no. variable name parameter no.
20592402 ctrlivar 824 ctrlivar 823
$.....$
*ctrlvar name type factor init f c
20592500 'i vlv xi' mult 1.0 0.0 0
*
*ctrlvar variable name parameter no. variable name parameter no.
20592601 ctrlivar 825 ctrlivar 824
$.....$
*ctrlvar name type factor init f c
20592600 'i stop v' stiffnctn 1.0 0.0 0
*
*ctrlvar function
20592601
*ctrlvar variable name parameter no. variable name parameter no.
20592602 ctrlivar 825 ctrlivar 826
$.....$
$ the turbine impulse pressure as a function of the turbine gate
$ valve area is calculated with the following control variables: the
$ pressure is specified by calculating the pressure drop across the
$ valve using the valve csurv, which is a linear function of the valve
$ normalized area (in this model).
$.....$
$ calculate the junction density in lbm/ft3.
$.....$
*ctrlvar name type factor init f c
20593000 'rhoj 804' mult 6.24798e-2 1.6214 1
*
*ctrlvar variable name parameter no. variable name parameter no.
20593001 voidf1 804000000 rhoj1 804000000
$.....$
*ctrlvar name type factor init f c
20593100 'rhoj 804' mult 6.24798e-2 0.03636 1
*
*ctrlvar variable name parameter no. variable name parameter no.
20593201 voidf1 804000000 rhoj1 804000000
$.....$
*ctrlvar name type factor init f c
20593200 'rho 804' sum 1.0 1.62776 1
*
*ctrlvar #0 coeff variable name parameter no.
20593201 0.0 1.0 ctrlivar 821
20593202 1.0 ctrlivar 822
$.....$
$ calculate q in gpm.
$.....$
*ctrlvar name type factor init f c
20593300 'q 804' div 386.55676 270820 1
*

```

```

*ctrlvar divisor name divisor no. dividend name dividend no.
20593401 ctrlivar 832 sflow2 804000000
$.....$
$ calculate the valve csurv using the the valve normalized area and
$ letnd with ctrlivar 824.
$.....$
*ctrlvar name type factor init f c min
20593400 'cv 804' mult 8257.2735 8257.2735 1.1 1.0e-9
*
*ctrlvar variable name parameter no.
20593401 ctrlivar 824
$.....$
$ divide C by csurv
$.....$
*ctrlvar name type factor init f c
20593500 'q/cv' div 1.0 82.3775 1
*
*ctrlvar divisor name divisor no. dividend name dividend no.
20593501 ctrlivar 834 ctrlivar 831
$.....$
$ square the result
$.....$
*ctrlvar name type factor init f c
20593600 '(q/cv)**2' power1 1.0 6785.904 1
*
*ctrlvar argument name argument no. int. point
20593601 ctrlivar 835 2
$.....$
$ multiply the result by the junction density and scale by 1/82.4
$.....$
*ctrlvar name type factor init f c
20593700 'delta p' mult 1.60256e-2 178.103 1
*
*ctrlvar variable name parameter no. variable name parameter no.
20593701 ctrlivar 832 ctrlivar 838
$.....$
$ calculate the unadjusted pressure in the turbine.
$.....$
*ctrlvar name type factor init f c
20593800 'p02 dp' sum 1.0 505.337 1
*
*ctrlvar #0 coeff variable name parameter no.
20593801 0.0 1.45037e-4 p 80201070
20593802 -1.0 ctrlivar 837
$.....$
$ adjust the calculated pressure for line losses and limit the result
$ to 15.553 psia.
$.....$
*ctrlvar name type factor init f c min max
20593900 'p turbine' sum 1.0 553.0 1.5 15.0 553.0
*
*ctrlvar #0 coeff variable name parameter no.
20593901 6.48762e-2 0.995075 ctrlivar 78
*
$.....$
$ end of example par relia5/end3 input model
$.....$
$ end of input

```



