NUREG/CR-3650 LA-10014-MS

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A Statistical Analysis of Nuclear Power Plant Pump Failure Rate Variability-Some Preliminary Results

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A Statistical Analysis of Nuclear Power Plant Pump Failure Rate Variability— Some Preliminary Results

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Manuscript submitted: January 1984 Date published: February 1984

Prepared for Division of Risk Analysis Office of Nuclear Regulatory Research US Nuclear Regulatory Commission Washington, DC 20555

NRC FIN No. A7725

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A STATISTICAL ANALYSIS OF NUCLEAR POWER PLANT PUMP FAILURE RATE VARIABILITY--SOME PRELIMINARY RESULTS

by

Harry F. Martz and David E. Whiteman

ABSTRACT

In-Plant Reliability Data System (IPRDS) pump failure data on over 60 selected pumps in four nuclear power plants are statistically analyzed using the Failure Rate Analysis Code (FRAC). A major purpose of the analysis is to determine which environmental, system, and operating factors adequately explain the variability in the failure data. Catastrophic, degraded, and incipient failure severity categories are considered for both demand-related and time-dependent failures.

For catastrophic demand-related pump failures, the variability is explained by the following factors listed in their order of importance: system application, pump driver, operating mode, reactor type, pump type, and unidentified plant-specific influences. Quantitative failure rate adjustments are provided for the effects of these factors.

In the case of catastrophic time-dependent pump failures, the failure rate variability is explained by three factors: reactor type, pump driver, and unidentified plant-specific influences.

Finally, point and confidence interval failure rate estimates are provided for each selected pump by considering the influential factors. Both types of estimates represent an improvement over the estimates computed exclusively from the data on each pump.

1. INTRODUCTION AND EXECUTIVE SUMMARY

Estimates of the reliability of numerous pump components are used in probabilistic risk analysis (PRA) of nuclear power plants. The estimates are used in quantifying the system fault tree models that appear in the event trees for each postulated accident.

The purpose of this report is (1) to determine the environmental, system, and operating factors which best explain (in a statistical sense) the observed differences in a certain set of estimated pump failure rates and to quantify the effects that these factors have on the failure rate estimates, (2) to determine various statistical models using the factors found in (1) which can be used to calculate pump failure rate estimates, and (3) to provide point and confidence interval estimates of pump failure rates using the models determined in (2).

Following the Introduction and Executive Summary in Section 1, Section 2 describes the pump failure rate data used in the analysis. Section 3 presents the detailed results of the analysis, which are summarized in Section 1.3. Finally, Section 4 gives the failure rate estimates.

1.1 Scope

The pump failure rate information analyzed here is the set of preliminary data for a selected group of important pumps identified and considered in the In-Plant Reliability Data System (IPRDS) on the pump component.¹ Pump data from four nuclear power plants are analyzed. The data cover 23 functionally different pumps for each of two Pressurized Water Reactors (PWRs), and 21 and 17 functionally different pumps, respectively, for two Boiling Water Reactors (BWRs). Because the data in Ref. 1 are assumed to be of a preliminary nature, the analysis undertaken here is likewise of a preliminary nature.

Two types of failures are analyzed: demand-related and time-dependent failures. Each pump is classified into one of three operating modes according to its primary mode of operation:

Running: The primary state of the pump is the running or active mode, for example, the condensate feedwater pumps.

Alternating: The pump alternates between the running and standby operating mode, such as boric acid transfer pumps.

Standby: The pump is normally in the standby state, for example, the containment spray pumps.

Pumps in the running mode have a time-dependent failure rate, while those in the standby mode possess a demand-related failure rate. Those in the alternating mode have both time- and demand-related failure rates.

One of three failure severity categories is assigned to each pump failure based on six possible failure mode categories. The three severity categories are

- Catastrophic: The pump is completely unable to perform its function. For example, the pump fails to start on demand.
- Degraded: The pump operates at less than its specified performance level. For example, there is low flow in the pump.

Incipient: The pump performs as designed but exhibits characteristics that, if left unattended, will likely develop into either a degraded or a catastrophic failure. For example, the pump mechanical seal leaks.

The six failure mode categories are fails to start, fails while running, low output, vibration, leakage, and other. A catastrophic failure is reported for a pump which either fails to start (for demand-related failures) or fails while running (for time-dependent failures). A degraded failure is reported when a pump fails in the low output mode, and an incipient failure occurs for those pumps failing in the vibration, leakage, or other failure mode categories.

A variety of factors are reported for each pump in the data base and several of these are considered here. Such factors as pump identification number, functional name, system and operating characteristics (such as pump and driver type, horsepower, and differential head), reactor type, plant designator, etc., are reported. However, in some cases not all of this information is readily available from the plant records, and the corresponding data fields have been left blank. Of all the factors reported,¹ six factors are complete enough to be considered here. They are

Reactor Type: Two types of light water reactors: (1) PWR and (2) BWR

- Plant: Four plants coded as (1) PWR No. 1, (2) PWR No. 2, (3) BWR No. 1, and (4) BWR No. 2
- System: The IPRDS data base considers pumps in the following seven systems: (1) Nuclear, (2) Engineered Safety, (3) Containment, (4) Electrical, (5) Power Conversion, (6) Process Auxiliary, and (7) Plant Auxiliary (Section 2 provides a generic listing of the plant systems in each of these categories)
- Operating Mode: Three dominant modes of pump operation: (1) Running, (2) Standby, and (3) Alternating
- Pump Type: Two major pump types: (1) Positive Displacement and (2) Centrifugal
- Pump Driver: Three types of pump drivers: (1) Motor, (2) Diesel, and (3) Turbine

For each failure severity category, the relationship is determined between each type of failure rate and the subset of the above factors found to be most statistically significant for explaining the variability in the failure rates. These relationships are used to calculate the numerical effect of each of the significant factors. The factors are also importance-ranked according to their effect on the failure rates.

1.2 Procedure

The Failure Rate Analysis Code $(FRAC)^2$ is used for the analysis. FRAC uses the well-established statistical methods of weighted least squares and weighted maximum likelihood to obtain the desired models based on the six factors previously discussed. The statistical significance level associated with a given model measures the ability of that model to explain the observed variability in the pump failure rate estimates. For a given failure rate type and severity category, finding the model having the smallest significance level, or P-Value, within the class of all feasible models is desirable. Such a model is subsequently identified and labeled the <u>Most Statistically Significant</u> (MSS) model. Although other models may do nearly as well in explaining the variability, none are better than the MSS model. The MSS model is considered here to be the best model, and the corresponding conclusions and estimates are based on this model.

In the past it has been customary to examine the effect of multiple factors on a failure rate one at a time. This is an inefficient method of analysis that does not lend itself to convenient investigation of interaction effects and may also indicate spurious effects when no such effects are present. Also, in such an analysis, often either failure rate estimates are given for each factor combination appearing in the data base with little or no data pooling or estimates are based on pooled data with little or no statistical assurance that such pooling is justified. In the case of little or no pooling, the estimates may be inefficient, while in the case of pooling, the estimates may be inappropriate or incorrect. For example, suppose that the effect of pump size on the failure rate is of interest. If data are pooled into each of several size categories, any apparent size effect may in fact be due to other factors which coincidentally correspond to the size categories. Such confounding effects can often result in confusing, and sometimes contradictory, reports regarding the factors that affect pump failure rates. This potentially inefficient and error-prone situation is avoided here by simultaneous consideration of all the factors in a statistical analysis of variance framework using FRAC. Because all the pump failure data are combined in the analysis, the point and interval estimates are expected to be superior to single-cell estimates such as reported by Drago et al. 1 This superiority is a direct consequence of the efficient FRAC method of analysis which permits all of the data to be simultaneously utilized. The FRAC model is briefly described in Section 3. Finally, FRAC pools data across one or more factors only if those factors have no clear, statistically discernible effect on the pump failure rate.

1.3 Conclusions

The following conclusions pertain to the ability of the six factors discussed in Section 1.1 to statistically account for and explain the observed variability in pump failure rates in the IPRDS pump failure data base.

Table I presents the MSS factors obtained from the FRAC analyses that explain the variability for both demand- and time-related catastrophic, degraded, and incipient failures. The factors are listed in their order of importance in explaining the variation. The level of statistical significance (the P-Value) associated with each set of factors is also given. Recall that each of these

P-Values is the smallest value within the class of all feasible combinations of the six main factors.

Table I also gives the percentage of the total pump variation that is explained by each of these MSS factors. In the case of both demand- and time-related catastrophic failures, significant plant-to-plant variation was found to be present; thus, a random factor, Plant, is included in the set of MSS factors. This factor accounts for those unidentifiable plant-to-plant differences in the pump failure rate not explainable by the other five factors.

In addition, Table I presents the best and worst values, in regard to the pump failure rate, for each fixed MSS factor. The actual quantitative adjustments corresponding to these best and worst case conditions, as well as all other remaining intermediate conditions, are given in Section 3 and the appendices.

The system application of a pump is an important factor that explains the variation in demand-related pump failure rates with Engineered Safety, Power Conversion, and Electrical systems projected to yield the smallest failure rates. The largest failure rates are expected to occur for Plant Auxiliary and Nuclear system applications. The pump driver is also an important factor. Together these two factors account for over 50% of the explainable catastrophic demand-related failure rate variability and 100% of the explainable degraded variability.

Reactor type is an important factor that explains the variation in time-dependent pump failure rates, with BWRs clearly projected to have the smallest failure rates. Pump driver is also an important explanatory factor for catastrophic and incipient time-dependent failure rate differences, with motor-driven pumps having the best projected rate of failure. Although the system application is by far the most important factor for the category of degraded pumps, it is not nearly as important for catastrophic or incipient time-dependent failures as it is for demand-related failures.

Finally, there is more unexplained variation in degraded pump failures than in either catastrophic or incipient failures. This is clear from the small P-Values for both the catastrophic and incipient cases.

TABLE I

MSS FACTORS AND THE PERCENTAGE OF PUMP FAILURE RATE VARIATION EXPLAINED BY EACH FIXED FACTOR

				Pump Fails	ure Rate	Percentage of Variation
Failure Type	Failure Severity	P-Value	MSS Factor	Best	Worst	Explained
Demand-Related	Catastrophic	0.28×10^{-8}	System	Eng. Safety	Plant Aux.	34
Demand-Related	Calastrophic	0.10	Pump Driver	Motor	Turbine	21
			Operating Mode	Alternating	Standby	20
			Reactor Type	BWR	PWR	13
			Pump Type	Pos. Disp.	Centrifugal	12
			Plant ^a			
	Degraded	0.17×10^{-2}	System	Power Conv.	Nuclear	73
			Pump Driver	Turbine	Diesel	27
	Inclutent	0.55×10^{-8}	System	Electrical	Plant Aux.	81
			Reactor Type	BWR	PWR	19
Time-Dependent	Catastrophic	0.96×10^{-7}	Reactor Type	BWR	PWR	53
True sependent			Pump Driver	Motor	Turbine	47
			Plant ⁸			
	Degraded	0.21×10^{-2}	System	Eng. Safety	Power Conv.	82
			Operating Mode	Running	Alternating	12
			Reactor Type	BWR	PWR	6
	Incipient	0.41×10^{-7}	Reactor Type	BWR	PWR	61
			Pump Driver	Motor	Turbine	39

aRandom factor.

2. IPRDS PUMP DATA BASE

The IPRDS pump data base includes more than 4 000 pump maintenance records on over 1 500 pumps for four nuclear power generating plants. These records span more than 27 plant-years of operation. Background information on the development of the IPRDS is given by Drago et al.³ The pump population data are taken directly from the plant equipment lists, and the failure data are taken from the maintenance records.

The pump boundary considers a "super" pump or pumping function. In addition to those failures of the pump itself, such as the pump impeller, shaft, or motor, local failures such as switches, local instrumentation, and control circuitry are also considered to be within the pump boundary. However, command faults such as loss of steam are not included in the pump boundary. The rationale for this approach is given in Drago et al.¹

From the population lists of pumps in the four plants, a set of over 60 important pumps was selected for reliability analysis by Drago et al.¹ This is the data set analyzed here. Tables II-V identify the selected pumps by plant. The entries in the column labeled "Population" are the number of pumps in the plant of that type. Definitions of the system codes in Tables II-V are given in Table VI.

The time-dependent and demand-related IPRDS pump failure data corresponding to Tables II-V are given in Appendix A. For simplicity, the following abbreviated names are used throughout this report for the six main factors listed in Section 1.1:

> RTYPE -- Reactor Type PLANT -- Plant SYSTEM -- System OPMODE -- Operating Mode PTYPE -- Pump Type DRIVER -- Pump Driver

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TABLE II

SELECTED PUMPS FROM PLANT 1: PWR

Functional Name	System Code	Pumpa, b Type	Driver Type	Population
Auxiliary feedwater (diesel)	\$05	С	D	1
Auxiliary feedwater (turbine)	S05	С	Т	1
Boric acid transfer	N09	с	м	2
Boron injection recirculation	N09	С	М	2
Centrifugal charging	N09	С	м	2
Circulating water	P06	С	м	2
Component-cooling water	W03	С	м	3
Condensate	P04	С	М	2
Containment spray	C10	с	М	2
Diesel fuel cil transfer	E04	С	м	2
Fire pump (motor)	X02	С	м	1
Fire pump (diesel)	X02	С	D	1
Fire system jockey pump	X02	С	М	1
F.W. pump turbine emergency lube oil	P05	PD	м	2
F.W. pump turbine lube oil transfer	P05	PD	м	1
F.W. pump turbine main lube of1	P05	PD	м	2
Positive displacement charging	N09	PD	М	1
Reactor coolant	N04	С	М	4
Residual heat removal	N08	С	М	2
Safety injection	S03	С	м	2
Service water	W04	С	М	3
Service water booster	W04	С	м	4
Steam generator feed F.W.	P05	С	Т	2

aC = centrifugal. bpD = positive displacement. cD = diesel. dM = motor. eT = turbine.

TABLE III

SELECTED PUMPS FROM PLANT 2: PWR

Functional Name	Code	Pump Type	Driver Type	Population
Auxiliary feedwater (motor)	S05	с	М	2
Auxiliary feedwater (turbine)	S05	С	Т	1
Boric acid transfer	N09	С	М	2
Boron injection recirculation	S03	С	М	2
Charging/high-head safety injection	N09	С	М	3
Chemical addition (continuous spray)	C10	С	М	1
Circulating water	P06	С	М	4
Component-cooling water	W03	С	М	3
Condensate	P04	С	М	2
Diesel-generator fuel oil transfer	E04	PD	М	4
Diesel-generator oil circulation	E04	С	М	2
Filtered seal water	W04	С	М	2
Fire pump (motor)	X02	PD	М	1
Fire pump (diesel)	X02	С	D	1
Fuel oil transfer	X02	PD	М	1
Low-head safety injection	S03	С	М	2
Inside recirculation spray	C10	С	М	2
Outside recirculation spray	C10	С	М	2
Quench spray	C10	С	м	2
Reactor coolant	N04	С	М	3
Residual heat removal	N08	С	М	2
Service water	W04	С	М	3
Steam generator feed	P05	С	М	2

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TABLE IV

SELECTED PUMPS FROM PLANT 3: BWR

Functional Name	System Code	Pump Type	Driver Type	Population
Condensate	P04	С	м	9
Condensate booster	P04	С	М	9
Condenser circulating	P06	С	М	9
Control rod drive	N02	С	М	5
Core spray	S03	С	М	12
Engine-driven fuel	E04	С	D	12
Fire	X02	С	3M,D	4
High-pressure coolant injection (HPCI)	S03	С	Т	3
HPCI booster	S03	С	Т	3
Lube oil transfer	E04	С	М	1
Raw cooling water	W03	С	М	12
Raw cooling water booster	W03	С	М	4
Reactor building closed cooling water	W03	С	М	9
Reactor core isolation cooling (RCIC)	S01	С	Т	3
Reactor feedwater	P05	С	Т	9
Reactor recirculating	N04	С	М	6
Residual heat removal	N08	С	М	12
Residual heat removal service water	W04	С	М	12
Seal water injection to F.W. pump	P05	С	М	6
Standby liquid control	N05	PD	м	6
Transfer pump	E04	С	М	22

TABLE V

SELECTED PUMPS FROM PLANT 4: BWR

Functional Name	System Code	Pump Type	Driver Type	Population
Circulating water	P06	с	м	4
Condensate	P04	С	М	3
Containment spray	C10	С	М	4
Control rod drive	N02	С	М	2
Core spray	S03	С	М	4
Core spray booster	S03	С	М	4
Diesel generator transfer	E04	С	М	4
Emergency diesel generator fuel	E04	PD	D	2
Emergency service water	W04	С	М	4
Fire (diesel)	X02	С	D	2
Fire jockey pump	X02	С	М	1
Reactor building closed cooling water	W03	С	М	2
Reactor feedwater	P05	с	М	3
Reactor recirculating	N04	С	М	5
Residual heat removal	N08	с	М	3
Service water	W04	с	М	2
Liquid poison (standby liquid control)	N05	PD	м	2

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TABLE VI

IPRD GENERIC SYSTEMS LIST

	Nuclear	Systems-N	
	BWR		PWR
NO1	Reactor core	NO1	Reactor core
N02	Control rod drive system	N02	Control rod drive system
N02.A	Control rod drive hydraulic system		
N03	Reactor control system	N03	Reactor control system
N04	Reactor recirculation system	N04	Reactor coolant system
N05	Standby liquid control system	N05	Emergency boration system
NOG	Reactor protection system	N06	Reactor protection system
N07	Neutron monitoring/nuclear instrumentation system	N07	Nuclear monitoring/nuclear instrumentation system
N08	Residual heat removal/low- pressure safety injection system	N08	Residual heat comoval/low- pressure safety injection system
N09	Reactor water cleanup system	N09	Chemical and volume control system (CVCS)

Engineered Safety Systems-S

	BWR		PWR
S01	Reactor core isolation cooling system		
		S02	Engineered safety features actuation system
S03	Engineered safety features	S03	Safety injection system
S03.A	High-pressure coolant injec- tion/core spray system	S03.A	High-pressure safety injec- tion subsystem
		S03.B	Safety injection tank/core flood subsystem
\$03.C	Low-pressure coolant injection	S03.C	Low-pressure safety injec- tion subsystem
S03.D	Low-pressure core spray system		
S03.E	Automatic depressurization system		
S04	Remote shutdown system	S04 S05	Remote shutdown system Auxiliary feedwater system

TABLE VI (cont)

Containment Systems-C

	BWR		PWR
C01	Primary containment and pene- trations		
C02	Reactor building	C02	Reactor building/containment and penetrations
C03	Containment heat removal	C03	Containment cooling system
		C03.A	Ice condenser system
C04	Containment isolation system	CO4	Containment isolation system
C05	Containment purge system	C05	Containment purge & stem
C06	Standby gas treatment system		
C07	Combustible gas control system	C07	Combustible gas control system
C08	Containment ventilation system	C08	Containment ventilation system
C09	Reactor building ventilation system		
C10	Containment spray system	C10	Containment spray system
		C11	Penetration room ventilation system

Electrical Systems-E

	BWR		PWR
E01 E01.A	Main power system Protective relaying and		 plant instrument ac power subsystem
	controls	E04	Emergency power system
E02	Plant ac distribution system	E04.A	Diesel-generator fuel oil
E02.B	Nonessential power system	EO4.B	Diesel-generator cooling water subsystem
E02.C	High-pressure core spray power system		
E02.D	Protective relaying and controls	E04.C	Diesel-generator air subsystem
E03	Instrumentation and control systems	EO4.D	Diesel-generator power lubrication oil
E03.A	dc power system		subsystem
	 vital dc power subsystem 	E05	Plant lighting system
	 plant dc power subsystem 	E05.A	Essential lighting
E03.B	Instrument ac power system	E05.B	Nonessential lighting
	 vital instrument ac power 	E06	Plant computer
	subsystem	E03.B	Instrument power system
		E07	Switchyard
		E07.A	dc control power system
		E07.B	Protective relaying

TABLE VI (cont)

Power Conversion Systems-P

	BWR		PWR
P01	Main steam system	P04.A	Condenser evacuation system
P02	Turbine-generator system	P04.B	Condensate cleanup/polishing
P02.A	Electro-hydraulic control		system
	subsystem	P04.C	Condensate heater drain
P02.B	Turbine gland seal subsystem		subsystem
P02.C	Turbine lubrication subsystem	P05	Feedwater system
P02.D	Stator (hydrogen) cooling subsystem	P05.A	Feedwater heater drain subsystem
P02.E	Hydrogen seal oil subsystem	P06	Circulating water system
P03	Turbine bypass system	P07	Steam generator blowdown (PWR)
P04	Condenser and condensate system	P08	Auxiliary steam system

Process /	Auxili	lary	Sy	st	ems-W

	BWR		PWR
W01	Radioactive waste system	W04.B	Station service water system
W01.A	 Gaseous radwaste system offgas subsystem (BWR) 		 essential service water system
WO1.B	Liquid radwaste system		 nonessential service
W01.C	Solid radwaste system		water system
W02	Radiation monitoring system		
W02.A	Plant area radiation monitors	W04.C	Chilled water system
W02.B	Environmental radiation	W05	Refueling system
	monitors	W06	Spent fuel storage system
W02.C W03	Process radiation monitors Cooling water systems	W06.A	Fuel-pool-cooling and clean- up systems
W03.A	Reactor building cooling	W07	Compressed air system
	water system	W07.A	Service air system
W03.B	Turbine building cooling	W07.B	Instrument air system
	water system	W08	Process sampling system
W04	Service water systems	W09	Plant gas system
W04.A	Demineralized makeup water	W09.A	Nitrogen system
	system	W09.B	Hydrogen system

Plant Auxiliary Systems-X

	BWR		PWR
X01	Potable and sanitary water system	X05.C	Diesel building ventilation system
X02 X02.A	Fire protection system Water system	X05.D	Auxiliary building ventila- tion system
X02.B X03	Carbon dioxide system Communications system	X05.E	Fuel building ventilation system
X04	Security system	X06	Nonradioactive waste system
X05	Heating, ventilating, and air conditioning systems	X06.A	Gaseous waste subsystem
X05.A	Control room habitability	X06.B	Liquid waste subsystem
	system	X06.C	Solid waste subsystem
X05.B	Turbine building ventilation system		

3. PUMP FAILURE RATE ANALYSIS

A short summary of the FRAC methodology is now given for background information. A complete description is provided by Martz, Beckman, and McInteer.²

A major assumption in the FRAC method is that all failure rates are constant during the time period for which the failure data have been collected. Thus, for any given pump (pump s for example), the number of failures of a given severity in time T_s follows a Poisson distribution with parameter $\lambda_s T_s$, where λ_s is the constant pump failure rate of interest, which is to be analyzed and estimated.

Suppose further that the true underlying failure rate λ_s is a function of K factors F_1, F_2, \ldots, F_k . The levels or values of factor F_j are denoted as $1, 2, \ldots, m_j$. For example, if F_1 denotes RTYPE, then F_1 has two levels: 1 for PWRs and 2 for BWRs. We denote the specific levels of the K factors associated with the sth pump failure data set in the data base (that is, the sth cell) as the set of pairs of indices $S = \{(1,s(1)), (2,s(2)), \ldots, (K,s(K))\}$, where s(j) is an integer from the set $\{1, 2, \ldots, m_j\}$. For example, if K = 3 then $S = \{(1,2), (2,3), (3,1)\}$ indicates that F_1 is at coded level 2, F_2 is at coded level 3, and F_3 is at coded level 1 for that cell.

The particular model adopted in FRAC for the failure rate $\boldsymbol{\lambda}_{g}$ associated with pump s is

 $\lambda_s = \lambda_g \prod_{j=1}^{K} A(j,s(j))$,

where A(j,s(j)) represents a multiplicative effect of factor F_j at the s(j)th level on the average failure rate λ_g . The A(j,s(j)) terms are thus multiplicative "adjustments" which account for the effect that factor F_j at level s(j) has on the average failure rate λ_g . The average failure rate λ_g acts as a constant term in the model and is the geometric average of all the pump failure rates in the data base.

The factors F_j may be either main factors, such as those listed in Section 1.1, or interactions of two or more main factors. However, no interactions are examined in this preliminary report because the number of pumps in the data base is insufficient to consider such interactions. The factors F_j may also be

either fixed (that is, nonrandom) factors or random variables. If F_j is a random factor, then log A(j,s(j)) is assumed to be the value of a normally distributed random variable with mean 0 and variance $\sigma_j^2/E(\lambda_g)T_g$; thus, A(j,s(j)) has a lognormal distribution with median one. In the FRAC analysis here, only the main factor PLANT is considered to be a random factor. The main reason for this is that the actual identity of each of the four plants represented in the data base is proprietary information and thus any PLANT effects cannot be attributed to specific plants. Therefore, any observed plant-to-plant differences for the four plants considered are interpreted as random plant population variability effects. If $\sigma_j^2 = 0$, then there is no PLANT effect on a given pump failure rate and A(j,s(j)) = 1 for all plants. However, if $\sigma_j^2 > 0$, then the larger the value of σ_j^2 , the greater the plant-to-plant contribution to the pump failure rate variability. The random factor PLANT thus represents the plant population variability effect on the pump failure rate.

3.1 Selecting the Best Model

FRAC uses the methods of weighted least squares and weighted maximum likelihood to arrive at estimates of the fixed effects A(j,s(j)) and the variance components σ_j^2 of the random factors. A chi-square statistic is computed and used to statistically assess the quality of fit of a given model to the observed pump failure rate data. For each model examined, the P-Value associated with the chi-square statistic is computed. This value is the probability of observing an associated chi-square statistic at least as large as the computed value by pure chance alone when only a constant term λ_g is in the model. For example, if the P-Value for a given model is 0.04, then the factors in the model (other than the constant term) are statistically able to explain the observed failure rate variability at the 4% level of significance. The smaller the P-Value, the more statistically significant the model. In other words, the smaller the P-Value, the better the set of factors in the given model can explain the observed variability in pump failure rates.

As discussed in Section 1.2, the class of models consisting of all feasible combinations of the six main factors given in Section 1.1 is considered. The model having the smallest P-Value within this class is labeled the Most Statistically Significant (MSS) model. This model is considered to be the best model for explaining the variability in the IPRDS pump failure rate data. All subsequent results, conclusions, and estimates are based on such MSS models.

Once the MSS model has been identified, the fixed factors in the model are ranked according to their overall effect in explaining the variability. The procedure is as follows: for a given fixed factor F_j , the ratio $R_j = \max_{s(j)} A(j,s(j))/\min_{j \in S} A(j,s(j))$ is computed. This ratio R_j measures the s(j) overall effect that F_j has on the average pump failure rate λ_g . The factors appearing in the MSS model are then ranked as follows: the factor having the largest R_j value is considered to be the most influential factor, the factor having the second largest R_j value is second most influential, and so on.

3.2 Demand-Related Failure Analysis

Recall from Section 1.1 that pumps which operate in either a standby or an alternating mode have an associated demand-related failure rate. We consider the catastrophic failure to start per demand as well as degraded and incipient failure rates per demand.

<u>3.2.1 Catastrophic Failures</u>. Table VII gives the P-Values for all feasible demand-related catastrophic FRAC failure rate models based on the six main factors. Because PLANT is nested within RTYPE, PLANT cannot appear in the model unless RTYPE is also present. The MSS model contains all six factors, and this model is highly statistically significant at the 0.28×10^{-8} level of significance. The outlined arrows in the table indicate the MSS model for a given number of factors, while the solid arrow indicates the overall MSS model.

Table VIII gives the estimated effects (the multiplicative "adjustments") for each of the factors at each possible level in the MSS model. The values of R_j are also given for each of the fixed factors, and the fixed factors in Table VIII are listed in their decreasing order of influence according to these values. The entries in parentheses in Table VIII are the estimated standard deviations associated with the estimated adjustments and variance components. The rather large standard deviations for some factor levels are the result of the relatively small quantity of data currently in the IPRDS pump failure data base for the selected group of pumps considered here.

The overall average pump failure rate estimate is 8.17×10^{-3} . This average value is roughly a factor of 8 larger than the commonly used WASH-1400 (Ref. 4) value of 10^{-3} per demand.

The factor SYSTEM is the most influential factor, having an overall range of effect of 2.79/0.38 = 7.34 on the average pump failure rate estimate. Plant Engineered Safety systems are estimated to have the smallest pump failure rates (an adjustment of 0.38), while pumps in Plant Auxiliary systems are estimated to have the largest failure rates (an adjustment of 2.79). Similarly, DRIVER is the second most influential factor; OPMODE is third; and so on.

The random factor PLANT is also in the MSS model. This means that there is statistically significant variability in pump failure rates between the two plants for each type of reactor which is not completely explained by the other five factors. However, it is not ranked because it is a random factor. The PLANT variance component in Table VIII will be reflected in the confidence interval estimates given in Section 4.

Table VIII can be used as follows: a centrifugally designed, standby, diesel-operated auxiliary feedwater pump in a PWR has an estimated catastrophic tailure rate per demand of

 $8.17 \times 10^{-3}(0.38)(0.71)(2.06)(1.67)(1.63) = 1.24 \times 10^{-2} \text{ f/d}$.

In performing a PRA the actual level of one or more of the factors in Table VIII may be either unknown or undetermined at the time the PRA is performed. In such case the corresponding factor adjustments could either simply be ignored, because the geometric mean of the adjustments for each fixed factor has a nominal value constrained to be equal to one, or the extreme adjustments corresponding to the unknown fixed factors could be used to establish a range of uncertainty due to the unknown factors.

Table IX gives the best and worst case catastrophic demand-related pump failure rate estimates based on the FRAC MSS model in Table VIII. There are approximately three orders of magnitude between the best and worst case estimates that are explained by the FRAC MSS model. This compares favorably with approximately 2.9 orders of magnitude between the largest and smallest failure rate estimates in the IPRDS demand-related data base in Appendix A. The observed range is expected to be smaller because the data extremes are unlikely to be the absolute best and worst case conditions, which may or may not represent feasible operating conditions. <u>3.2.2 Degraded Failures</u>. Table B-I in Appendix B gives the P-Values for all feasible degraded FRAC failure rate models based on the six main factors. The dashes (--) in Table B-I indicate those models in which it is not possible to consider all the indicated factors, primarily the result of "multi-collinearity" between the factors. Such models are thus infeasible. In such cases FRAC "zeros out" one or more of the collinear factors, and the corresponding model reduces to one of the lower order models in the table. The MSS model contains the two factors SYSTEM and DRIVER and is highly significant at the 1.67×10^{-3} level of significance.

Table B-II gives the multiplicative adjustments for each of the two factors in the MSS model. Analogous to Table VIII, Table B-II lists the factors in their decreasing order of influence according to the value of R_j . SYSTEM is the most influential factor with a range of 28, nearly three times that of the remaining factor, DRIVER. Pumps in Nuclear systems are expected to have the largest degraded demand-related failure rates, while pumps in Power Conversion systems are expected to have the smallest failure rates.

Table B-III gives the best and worst case failure rate estimates based on the FRAC model in Table B-II. There are approximately 3.5 orders of magnitude between the best and worst case estimates that are accounted for by the FRAC MSS degraded demand-related pump failure rate model.

<u>3.2.3 Incipient Failures</u>. Tables B-IV through B-VI give the results of the pump demand-related FRAC failure rate analysis for incipient failures. Table B IV gives the P-Values for all feasible FRAC models using the six main factors. The MSS model contains the two factors SYSTEM and RTYPE and is highly significant at the 5.55×10^{-9} level of significance.

Table B-V gives the multiplicative adjustments. The factor SYSTEM is the most influential factor with a range of effect slightly over an order of magnitude, while RTYPE has a range of 2.90. Because incipient failures are often precursors of either catastrophic or degraded failures, incipient pump failures in Plant Auxiliary, Nuclear, Process Auxiliary, and Engineered Safety systems should be carefully monitored as possible precursors of more serious pump failures which may jeopardize plant safety.

Table B-VI gives the best and worst case FRAC estimates using the model in Table V. There are roughly 1.6 orders of magnitude between the best and worst case estimates that are explainable by the FRAC MSS model.

3.3 Time-Dependent Failure Analysis

Recall that pumps which operate in either a running or alternating mode have an associated time-related failure rate. We consider the catastrophic failure rate per operating hour as well as the degraded and incipient failure rates per hour of operation.

<u>3.3.1 Catastrophic Failures</u>. Table X gives the P-Values for all feasible time-dependent catastrophic FRAC failure rate models. The MSS model contains only the two factors RTYPE and DRIVER and is highly significant at the 9.6×10^{-8} level.

The estimate of the average pump failure rate λ_g is 8.91 × 10⁻⁵ per operating hour and is roughly three times larger than the corresponding WASH-1400 (Ref. 4) value of 3 × 10⁻⁵ per operating hour.

Table XI gives the multiplicative adjustments for the FRAC MSS model. The range of effect of both factors is approximately four, which indicates that there is less variability in the catastrophic time-dependent pump failure rate data base than in the demand-related data base. Also, the FRAC MSS model in Table XI explains less variability than the model in Table VIII as demonstrated by the rather large error variance component in Table XI. This may also be seen in Table XII in which only 1.3 orders of magnitude separate the best and worst case estimates produced by the FRAC MSS model. Recall that in the case of catastrophic demand-related estimates, this difference was over three orders of magnitude.

<u>3.3.2 Degraded Failures</u>. Table C-I in Appendix C gives the P-Values for all feasible time-dependent degraded FRAC failure rate models. The MSS model contains three factors, SYSTEM, OPMODE, and RTYPE, and this model is statistically significant at the 0.0021 level of significance.

Table C-II gives the multiplicative failure rate adjustments for the MSS model. SYSTEM is the most important factor, having a tange of effect of 33.40. This range is nearly 7 times that of the second most important factor, OPMODE, and nearly 15 times that of the third most influential factor, RTYPE.

Table C-III gives the best and worst case FRAC estimates based on the MSS model in Table C-II. The FRAC MSS model yields an overall range of variability of approximately 2.6 orders of magnitude between the best and worst case estimates.

<u>3.3.3 Incipient Failures</u>. Table C-IV gives the P-Values for all the feasible FRAC models based on the six main factors. The MSS model contains the two factors, RTYPE and DRIVER.

Table C-V gives the estimated failure rate adjustments for the MSS model. Note that neither RTYPE nor DRIVER has a large range of effect on the incipient time-dependent pump failure rates. Although RTYPE has the larger R_j value, it is only slightly more influential than DRIVER.

Table C-VI gives the best and worst case estimates using the FRAC MSS model in Table C-V. Only a 0.9 order of magnitude separates these estimates. Incipient failures in PWR turbine driven pumps should be carefully monitored as possible precursors of either catastrophic or degraded failures that may jeopardize plant safety.

TABLE VII

CATASTROPHIC DEMAND-RELATED FRAC FAILURE RATE MODEL ANALYSIS

One-Factor Models

RTYPE SYSTEM OPMODE PTYPE DRIVER

Two-Factor Models

RTYPE, PLANT
RTYPE, SYSTEM
RTYPE, OPMODE
RTYPE, PTYPE
RTYPE, DRIVER
SYSTEM, OPMODE
SYSTEM, PTYPE
SYSTEM, DRIVER
OPMODE, DRIVER
OPMODE, PTYPE
DEVER DETURE

	-		-
0.2338	×	10-2	
0.1164	×	10-3	<
0.1510	×	10-2	
0.4767	×	100	
0.4431	×	10-2	

P-Values

P-Values

 0.7798×10^{-2} 0.4179×10^{-5} 0.1999×10^{-4} 0.7810×10^{-2} 0.2644×10^{-3} 0.1304×10^{-4} 0.2316×10^{-3} 0.4966×10^{-4} 0.7896×10^{-3} 0.2199×10^{-2} 0.1178×10^{-1}

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1 m

TABLE VII (cont)

Three-Factor Models

RTYPE, PLANT, SYSTEM RTYPE, PLANT, OPMODE RTYPE, PLANT, DTYPE ETYPE, PLANT, DRIVER RTYPE, SYSTEM, OPMODE RTYPE, SYSTEM, DTYPE RTYPE, SYSTEM, DRIVER RTYPE, PTYPE, SYSTEM PTYPE, SYSTEM, OPMODE DRIVER, OPMODE, SYSTEM OPMODE, PTYPE, DRIVER RTYPE, PTYPE, OPMODE RTYPE, DRIVER, OPMODE SYSTEM, DRIVER, PTYPE

Four-Factor Models

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RTYPE, PLANT, SYSTEM, OPMODE RTYPE, PLANT, SYSTEM, PTYPE RTYPE, PLANT, SYSTEM, DRIVER RTYPE, PLANT, OPMODE, PTYPE RTYPE, PLANT, OPMODE, DRIVER RTYPE, PLANT, PTYPE, DRIVER SYSTEM, RTYPE, DRIVER, OPMODE RTYPE, PTYPE, DRIVER, SYSTEM PTYPE, SYSTEM, OPMODE, RTYPE DRIVER, OPMODE, RTYPE, PTYPE OPMODE, PTYPE, DRIVER, SYSTEM

Five-Factor Models

RTYPE, PLANT, SYSTEM, OPMODE, PTYPE RTYPE, PLANT, SYSTEM, OPMODE, DRIVER RTYPE, PLANT, SYSTEM, DRIVER, PTYPE RTYPE, PLANT, OPMODE, PTYPE, DRIVER RTYPE, SYSTEM, PTYPE, DRIVER, OPMODE

Six-Factor Model

RTYPE, PLANT, SYSTEM OPMODE, PTYPE, DRIVER

0.3305	×	10 ⁻⁵	
0.4520	×	10-4	
0.1504	×	10 ⁻¹	
0.2487	×	10-3	
0.7428	×	10-7	<
0.1029	×	10-4	
0.6813	×	10 ⁻⁶	
0.7312	×	10-3	
0.7840	×	10-5	
0.5338	×	10 ⁻⁵	
0,1201	×	10^2	
0.2536	×	10-4	
0.2293	×	10-4	
0.1000	×	10-3	

P-Values

P-Values

		-6	
0.1105	×	10-0	
0.7688	×	10-5	
0.4720	×	10 ⁻⁶	
0.2641	×	10-4	
0.5359	×	10-4	
0.6670	×	10-3	
0.7980	×	10-8	<
0.1697	×	10-5	
0.5595	×	10-7	
0.3529	×	10-4	
0.3647	×	10-5	

P-Values

0,2011	×	10-7	
0.1140	×	10-7	
0.1094	×	10 ⁻⁵	
0.5185	×	10-4	
0.6403	×	10-8	4
P-Value	es		

 0.2784×10^{-8}

TABLE VIII

CATASTROPHIC DEMAND-RELATED MSS FRAC MODEL

Average Failure Rate Estimate--8.17 \times 10⁻³ (2.60 \times 10⁻³)

11	xed	raci	tors
	12.00 1.4	A CALL	LOLD.

Level of Influence	Factor	Level	Description	Rj	Failure Rate Adjustment
1	SYSTEM	1	Nuclear	7.34	2.66 (0.636)
		2	Engineered Safety		0.38 (0.131)
		3	Containment		0.64 (0.228)
		4	Electrical		0.53 (0.177)
		5	Power Conversion		0.57 (0.397)
		6	Process Auxiliary		1.84 (0.484)
		7	Plant Auxiliary		2.79 (0.718)
2	DRIVER	1	Motor	4.48	0.56 (0.114)
		2	Diesel		0.71 (0.189)
		3	Turbine		2.51 (0.849)
3	OPMODE	1	Standby	4.20	2.06 (0.302)
		2	Alternating		0.49 (0.071)
4	RTYPE	1	PWR	2.78	1.67 (0.298)
		2	BWR		0.60 (0.107)
5	PTYPE	1	Positive Displacement	2.67	0.61 (0.117)
		2	Centrifugal		1.63 (0.312)

Random Factors

Factor	Variance Component
PLANT	0.882 (0.0854)
ERROR	0.586 (0.1061)

TABLE IX

BEST AND WORST CASE CATASTROPHIC DEMAND-RELATED FRAC PUMP FAILURE RATE ESTIMATES

CASE	SYSTEM	DRIVER	OPMODE	RTYPE	РТҮРЕ	ESTIMATE
Best Worst	Eng. Safety Plant Aux.	Motor Turbine	Alternating Standby	BWR PWR	Pos. Displacement Centrifugal	$3.09 \times 10^{-4}/d$ $3.21 \times 10^{-1}/d$
Note:	3.21×10^{-1}	/3.09 × 1	$0^{-4} = 1039 \simeq$	3.0 ord	ers of magnitude be	etween the best

and worst case estimates.

TABLE X

CATASTROPHIC TIME-DEPENDENT FRAC FAILURE RATE MODEL ANALYSIS

One-Factor Models

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RTYPE SYSTEM OPMODE PTYPE DRIVER

Two-Factor Models RTYPE, PLANT RTYPE, SYSTEM RTYPE, OPMODE RTYPE, PTYPE RTYPE, DRIVER SYSTEM, OPMODE SYSTEM, DRIVER OPMODE, DRIVER OPMODE, PTYPE PTYPE, DRIVER

P-Value	s		
0.8883	×	10 ⁻⁴	1
0.7802	×	10 ⁻²	Y
0.1379	×	100	
0.5759	×	100	
0.9651	×	10 ⁻¹	

-
(
Y

TABLE X (cont)

Three-Factor Models

RTYPE, PLANT, SYSTEM RTYPE, PLANT, OPMODE RTYPE, PLANT, DTYPE RTYPE, PLANT, DRIVER RTYPE, SYSTEM, OPMODE RTYPE, SYSTEM, DTYPE RTYPE, SYSTEM, DRIVER RTYPE, SYSTEM, OPMODE DRIVER, OPMODE, SYSTEM OPMODE, PTYPE, DRIVER RTYPE, PTYPE, OPMODE RTYPE, DRIVER, OPMODE SYSTEM, DRIVER, PTYPE

Four-Factor Models

RTYPE, PLANT, SYSTEM, OPMODE RTYPE, PLANT, SYSTEM, PTYPE RTYPE, PLANT, SYSTEM, DRIVER RTYPE, PLANT, OPMODE, PTYPE RTYPE, PLANT, OPMODE, DRIVER RTYPE, PLANT, PTYPE, DRIVER SYSTEM, RTYPE, DRIVER, OPMODE RTYPE, PTYPE, DRIVER, SYSTEM PTYPE, SYSTEM, OPMODE, RTYPE DRIVER, OPMODE, RTYPE, PTYPE OPMODE, PTYPE, DRIVER, SYSTEM

Five-Factor Models

RTYPE, PLANT, SYSTEM, OPMODE, PTYPE RTYPE, PLANT, SYSTEM, OPMODE, DRIVER RTYPE, PLANT, SYSTEM, DRIVER, PTYPE RTYPE, PLANT, OPMODE, PTYPE, DRIVER RTYPE, SYSTEM, PTYPE, DRIVER, OPMODE

Six-Factor Model

RTYPE, PLANT, OPMODE SYSTEM, PTYPE, DRIVER

P-Valu	es		_
		11.1	
0.4424	×	10-4	
0.1319	×	10-3	
0.3063	×	10-3	
0.9622	×	10 ⁻⁷	4
0.3437	ж	10-4	
0.5850	×	10-4	
0.1461	×	10-4	
0,1166	×	10-4	
0.2904	*	10-1	
0.2355	×	10-1	
0.2985	×	100	
0.2538	×	10-3	
0.2253	×	10-4	
0.3206	×	10 ⁻¹	

P-Values

0.4646	×	10-4
0.8078	×	10-4
0.1468	×	10 ⁻⁵
0.2085	×	10 ⁻³
0.3374	×	10-6
0.2880	×	10-6
0.1008	×	10-4
0.2474	×	10-4
0.8019	×	10-4
0.4021	×	10-4
0.4615	×	10-1

P-Value	e		
0.1044	×	10-3	
0.6739	×	10 ⁻⁶	
0.3154	×	10 ⁻⁵	4
0.9006	×	10-6	
0.2370	×	10-4	

P-Value

0.1735 × 10⁻⁵

TABLE XI

CATASTROPHIC TIME-DEPENDENT MSS FRAC MODEL

Average Failure Rate Estimate -- 8.91×10^{-5} (2.63 × 10^{-5})

Fixed Factors

			and the state of the state			
evel of influence	Factor	Level	Description	Rj	Failure Rate Adjustment	-
1	RTYPE	1 2	PWR BWR	4.57	2.15 (0.608) 0.47 (0.132)	1
2	DRIVER	1 2	Motor Turbine	3.98	0.50 (0.071) 1.99 (0.278)	
		Ra	ndom Factors			
	Factor			Varian	ce Component	
	PLANT			0.26	9 (0.225)	

TABLE XII

BEST AND WORST CASE CATASTROPHIC TIME-DEPENDENT FRAC PUMP FAILURE RATE ESTIMATES

Case	RTYPE	DRIVER	Estimate			
Best	BWR	Motor	$2.09 \times 10^{-5}/h$			
Worst	PWR	Turbine	$3.81 \times 10^{-4}/h$			

Note: $3.81 \times 10^{-4}/2.09 \times 10^{-5} = 18.23 \approx 1.3$ orders of magnitude between the best and worst case estimates.

4. PUMP FAILURE RATE ESTIMATES

Point estimates of pump failure rates are calculated directly from the estimated FRAC MSS models, such as in Tables VIII and XI. Confidence interval estimates are computed using the FRAC procedure and equations given in Martz, Beckman, and McInteer.² Estimates are given for each of the pump failure data entries in the data bases in Appendix A. Ninety-five percent confidence interval estimates are given in which the lower and upper interval endpoints correspond to the lower 2.5% and upper 97.5% confidence limits, respectively, on the corresponding true (but unknown) underlying pump failure rate.

For convenience, the following coded abbreviations are used in the tables which follow:

 $\frac{\text{RTYPE}}{\text{P} = \text{PWR}}$ B = BWR

PLANT

1	-	Plant	1	(PWR)
2	=	Plant	2	(PWR)
3	=	Plant	3	(BWR)
4	=	Plant	4	(BWR)

OPMODE

S	=	Standby
А		Alternating
R	-	Running

DRIVER

M = Motor D = Diesel T = Turbine

PTYPE

PD = Positive Displacement

C = Centrifugal

Tables XIII-XV give the point and 95% confidence interval estimates of the demand-related pump failure rates for catastrophic, degraded, and incipient failure severity categories for each pump in Table A-II. The point estimates are the "recommended" values, while the lower and upper interval endpoints are considered to be the "low" and "high" values, respectively. The SYSTEM codes are defined in Table VI. The estimates are given as failures per demand. Different failure rate estimates are obtained only for different levels or values of the MSS factors, as these are the only factors that appear in the corresponding MSS models.

Consider the first entry in Table XIII, the catastrophic failure rate per demand for a PWR centrifugally designed, diesel-operated, standby auxiliary feedwater pump. The point estimate is $1.2.5 \times 10^{-2}$ per demand. The corresponding single-cell point estimate based on one catastrophic failure in 60 demands is $1/60 = 1.67 \times 10^{-2}$. The FRAC MSS model estimate is thus roughly 75% as large as the simple single-cell estimate. This reduction is the result of considering additional failure data for the other pumps in the data base via the FRAC MSS model. Now consider the 95% confidence interval estimate. The FRAC estimate based on the chi-square distribution, such as given by Drago et al.,¹ is $(4.25 \times 10^{-4}, 9.29 \times 10^{-2})$. The FRAC interval estimate is roughly 32 times narrower than the single-cell estimate. This reduction in uncertainty is also the result of the pooled utilization of all the pump failure data via the FRAC MSS model.

Similarly, Tables XVI-XVIII give the estimates of the time-dependent pump failure rates for each pump entry in Table A-IV.

TABLE XIII

CATASTROPHIC DEMAND-RELATED FRAC PUMP FAILURE RATE ESTIMATES PER DEMAND

234	AUX FW	P	1	S	Ð	C	505	0.1249E-01	(0.4777E-02.0.3265E-01)
234	ALIX FW	-							
3 4	MUCH FR	P	1	S	T	C	\$05	0.4387E-01	(0.1951E-01.0.9866E-01)
4	RORIC ACID TRANSFER	D	4		8.0	0	NICO	0 16025-01	(0 8863E-02 0 2898E-01)
. 4	DODON THISOTION DECTRON ATTON	-	1.2	-	141	-	140.9	0.10032-01	(0.00000 02,0.20000 01)
-	BURUN INVECTION RECIRCULATION	٣.	-31	A	M	C	NOA	0.16032-01	(0.88632-02,0.28982-01)
5	CENTRIFUGAL CHARGING	P	÷.,	S	M	C	NO9	0.6818E-01	(0.3318E-01,0.1401E+00)
6	COMPONENT-COOLING WATER	P	1	Δ	M	C	WO3	0.1105E-01	(0.5673E-02.0.2154E-01)
7	CONTAINMENT SPRAV	D		<	8.6	C	C10	0 16485-01	(0 7326E-02 0 3709E-01)
0	DIECEL EUEL OIL TRANCEED	5		2		~	504	0.10400 01	
0	DIESEL FUEL UIL INANSFER	٢	1.1	2	M	0	EO4	0.13598-01	(0.58286-02,0.31696-01)
9	FIRE	P	1	S	M	C	XO2	0.7138E-01	(0.3710E-01,0.1373E+00)
10	FIRE	P	1	S	D	C	X02	0.9138E-01	(0.4734E-01.0.1764E+00)
11	FIRE JOCKEY	D	4.1	č	M	0	XO2	0 71385-01	(0 3710E-01 0 1373E+00)
10	EW TUDDINE ENED LUDE OT	-		2	141	00	NUE	0. 1000 01	(0. 31 10E 01, 0. 107 5E 00)
12	FW TURDING EMER LUDE UIL	P	1	5	M	PD	P05	0.5434E-02	(U. 1108E-Uz, U. 2000E-UT)
13	FW TURBINE LUBE OIL TRANSFER	P	1	S	M	PD	PO5	0.5434E-02	(0.1108E-02.0.2666E-01)
14	RESIDUAL HEAT REMOVAL	P	1	Δ	M	C	NO8	0.1603E-01	(0.8863E-02.0.2898E-01)
15	SAFETY INJECTION	D		C	8.6	c	502	0 97565-02	(0 4201E-02 0 2266E-01)
+0	CEDVICE WATED	-				0	303	0.01000 02	(0, 42012 02, 0, 22002 01)
10	DERVICE WATER	P	3	A	M	C	W04	0.1105E-01	(0.56/32-02,0.21542-01)
17	SERVICE WATER BOOSTER	P	1	A	M	C	WO4	0.1105E-01	(0.5673E-02,0.2154E-01)
18	AUX FW	P	2	S	M	C	505	0.9756E-02	(0.4201E-02.0.2266E-01)
19	AUX FW	P	2	S.	T	C	505	0 43875-01	(0 1951E-01 0 9866E-01)
00	DODIC ACTO TRANSFER	-	-	-	in the	~	300	0.40072 01	(0. 1001E 01, 0. 0000E 01)
20	BURIC ACIU INANDEER	2	4	A	M	C	NOS	0.1603E-01	(0.8863E-02.0.2898E-01)
21	BORON INJECTION RECIRCULATION	P	2	A	M	C	SO3	0.22935-02	(0.8713E-03,0.6037E-02)
22	CHARGING/HIGH-HEAD SAFETY INJECTION	P	2	Δ	M	C	NO9	0.1603E-01	(0.8863E-02.0.2898E-01)
23	CHEMICAL ADDITION (CONTAINMENT SPRAV)	D	2	C	8.6	č	010	0 16495-01	(0 7326E-02 0 3/09E-01)
5.4	COMOQUENT COOL THE WATER	-	~	3	100	~	010	0.10462-01	(0. 7520E 02.0.0705E 01)
24	CUMPUNENT-CUULING WATER	٣	2	A	M	C	MO3	0.1105E-01	(0.56/3E-02,0.2154E-01)
25	DIESEL-GENERATOR FUEL OIL TRANSFER	P	2	S	M	PD	EO4	0.5088E-02	(0.1851E-02.0.1399E-C1)
26	DIESEL-GENERATOR OIL CIRCULATION	P	2	S	M	PD	EO4	0.5088E-02	(0.1851E-02.0.1399E-01)
27	FILTERED SEAL WATER	D	2	٨	8.4	C	WOA	0 11055-01	(0 5673E-02 0 2154E-01)
20	ETDE		-	2			W04	0.11002-01	(0.00/00 02,0.21040 01)
28	FIRC	٣	2	2	M	PD	X02	0.2673E-01	(0.10392-01,0.68/32-01)
29	FIRE	P	2	S	D	C	XO2	0.9138E-01	(0.4734E-01,0.1764E+00)
30	FUEL DIL TRANSFER	P	2	S	M	PD	X02	0.2673E-01	(0.1039E-01.0.6873E-01)
31	LOW HEAD SAFETY IN JECTION	P	2	C	M	C	503	0 97565-02	(0 A201E-02 0 2266E-01)
50	TNETDE DECTOCULATION CODAV	2	-	5		~	505	0.37300-02	(0.4201L 02.0.2200L 01)
32	INSIDE REGIRCOLATION SPRAT	2	4	2	M	6	610	0.16486-01	(0.7326E-02,0.3709E-01)
33	OUTSIDE RECIRCULATION SPRAY	P	2	S	M	C	C10	0.1648E-01	(0.7326E-02,0.3709E-01)
34	QUENCH SPRAY	P	2	S	M	C	C10	0.1648E-01	(0.7326E-02.0.3709E-01)
35	RESIDUAL HEAT REMOVAL	p	2	۸	M	C	NOR	0 16035-01	(0.8863E-02 0.2898E-01)
26	CEDVICE WATED		2	7		~	HOA	0.10050 01	(0,0000E 02,0,2000E 01)
30	SERVICE WATER	"	*	A	M	6	WO4	0.1105E-01	(0.56/32-02.0.21542-01)
37	CONTROL ROD DRIVE	В	3	A	M	C	NO2	0.5759E-02	(0.3041E-02,0.1091E-01)
38	CORE SPRAY	B	3	S	M	C	503	0.3505E-02	(0.1498E-02.0.8202E-02)
39	ENGINE-DRIVEN FUEL	R	3	S	D	C	FO4	0 62515-02	(0.2354E-02 0.1660E-01)
40	FIDE	D	2	č	M	č	xoo	0.02012 02	(0 12425-01 0 40025-01)
40	FIRE	2	3	2	m.	6	X02	0.25652-01	(0.1342E-01.0.49C2E-01)
41	HIGH-PRESSURE COULANT INJECTION	В	3	S	Т	C	203	0.1576E-01	(0.7307E-02,0.3400E-01)
42	HPCI BODSTER	B	3	S	T	C	503	0.1576E-01	(0.7307E-02.0.3400E-01)
43	LUBE DIL TRANSFER	R	3	S	M	C	FO4	0 48835-02	(0 2098E-02 0 1136E-01)
4.4	DAW COOLING WATED	D	2			~	woa	0. 20705 - 02	(0.2460E-02.0.707EE-02)
45	ANY COULING WATER BOOSTED	0	3	A	141	6	w03	0.39726-02	10.21092-02.0.12132-021
45	RAW CUULING WATER BOUSTER	В	3	A	M	C	MO3	0.3972E-02	(0.2169E-02,0.7275E-02)
46	REACTOR BUILDING CLOSED COOLING	B	3	A	M	C	WO3	0.3972E-02	(0.2169E-02.0.7275E-02)
47	REACTOR CORE ISOLATION COOLING	R	3	5	T	C	501	0 1576F-01	(0 7307E-02 0 3400E-01)
40	DESTDUAL WEAT DEMOVAL		3			~	NOR	0 57505-00	(0. 2044E-02. 0. 1004E-01)
40	RESIDUAL HEAT REMOVAL	0	2	-	m	6	NUB	0.5/592-02	(U. 3041E-02. U. 1091E-01)
49	RMR SERVICE WATER	В	3	A	M	C	WO4	0.3972E-02	(0.2169E-02,0.7275E-02)
50	SEAL WATER INJECTION TO FW	B	3	Α	M	C	POS	0.1226E-02	(0.2288E-03.0.6569E-02)
51	LIQUID CONTROL	R	3	5	M	PD	NOS	0 9172E-02	(0 4112E-02 0 2046E-01)
60	TDANCEED	ñ	2	ē		~	FOA	0 10025 00	(0. 2000E-02. 0. 112EE-01)
94	INANDEEK	0	3	2	m	0	EU4	0.4883E-02	10.20986-02.0.11366-011
53	CONTAINMENT SPRAY	B	4	S	M	C	C10	0.5923E-02	(0.2593E-02.0.1353E-01)
54	CONTROL ROD DRIVE	8	4	Δ	M	C	NO2	0.5759E-02	(0.3041E-02.0.1091E-01)
55	CORF SPRAV	R	4	5	M	c	503	0 35055-02	(0 1498E-02 0 8202E-02)
50	CORE CORA DOGETED	0	-	0		5	505	0.35056-02	(0. 14506 02,0.02026 02)
20	CURE SPRAY BUUSIER	В	4	5	M	C	503	0.3505E-02	(0.1498E-02.0.8202E-02)
57	DIESEL-GENERATOR TRANSFER	в	4	S	D	C	EO4	0.6251E-02	(0.2354E-02.0.1660E-01)
58	EMER DIESEL-GENERATOR FUEL	8	4	S	D	PD	EQ4	0.2341E-02	(0.7343E-03.0.7461E-02)
50	EMED SERVICE WATER	R		c		0	WOA	0 16905-01	(0 REGIE 02 0 20055 01)
20	ETDE	2	-	5	1	0	W04	0.10502-01	(0.0001L 02.0.0200E 01)
00	LIKE	0	4	2	0	C	X02	0.3283E-01	(0.1628E-01,0.6622E-01)
61	FIRE JOCKEY	B	4	S	M	C	XO2	0.2565E-01	(0.1342E-01,0.4902E-01)
62	REACTOR BUILDING CLOSED COOLING	B	4	Δ	M	C	WO3	0.3972E-02	(0,2169E-02,0,7275E-02)
52	PESTDUAL HEAT PEMOVAL	R	1		M	r	NOR	0 57595-00	(0 3041E-02 0 1001E-01)
6.4	CEDUTCE WATED	0	-	-		č	WOA	0.0705-02	(0.000 E 02.0. 100 E 01)
0.4	SERVICE WATER	В	4	A	M	C	WO4	0.3972E-02	(0.2169E-02.0.7275E-02)
EX EX	LIGHTO CONTROL (POISON)	B	4	S	M	PD	NO5	0.9172E-02	(0.4112E-02.0.2046E-01)

TABLE XIV

DEGRADED DEMAND-RELATED FRAC PUMP FAILURE RATE ESTIMATES PER DEMAND

. 1	AUX FW	P	1	S	D	С	S05	0.1478E+00	(0.6088E-01.0.3587E+00)
2	AUX FW	P	1.	S	Т	C	S05	0.1414E-01	(0.2800E-02.0.7141E-01)
3	BORIC ACID TRANSFER	P	1	A	M	C	NO9	0.7459E-01	(0.4570E-01,0.1217E+00)
4	BORON INJECTION RECIRCULATION	P	1	Α	M	C	NOS	0.7459E-01	(0.4570E-01,0.1217E+00)
5	CENTRIFUGAL CHARGING	P	1	S	M	С	NO9	0.7459E-01	(0.4570E-01.0.1217E+00)
6	COMPONENT-COOLING WATER	P	1	Α	M	C	WO3	0.3135E-01	(0.1905E-01,0.5158E-01)
7	CONTAINMENT SPRAY	P	1	S	M	C	C10	0.5800E-02	(0.4888E-03,0.6882E-01)
8	DIESEL FUEL OIL TRANSFER	P	1	S	M	C	EO4	0.5120E-02	(0.1067E-02.0.2458E-01)
9	FIRE	P	1	S	M	C	X02	0.1955E-01	(0.6145E-02.0.6222E-01)
10	FIRE	P	1	S	D	C	X02	0.6457E-01	(0.1338E-01,0.3116E+00)
11	FIRE JOCKEY	P	1	S	M	C	X02	0.1955E-01	(0.6145E-02.0.6222E-01)
12	FW TURBINE EMER LUBE OIL	P	1	S	M	PD	PO5	0.2705E-02	(0.81818-04,0.89418-01)
13	FW TURBINE LUBE OIL TRANSFER	P	1	S	M	PD	P05	0.2705E-02	(0.81812-04,0.89412-01)
14	RESIDUAL HEAT REMOVAL	P	1	A	M	C	80M	0.74598-01	(0.45702-01.0.12172+00)
15	SAFETY INJECTION	P	1	S	M	C	503	0.44/56-01	(0.102/E-01,0,1949E+00) (0.1025E-01,0,1949E+00)
16	SERVICE WATER	P	1	A	M	0	WO4	0.31356-01	(0.1905E-01,0.5158E-01)
17	SERVICE WATER BOUSTER	P	1	A	M	C	WQ4	0.31356-01	(0.1007E-01.0.104949E+00)
18	AUX FW	P	2	5	T N	0	505	0.44752-01	(0 2800E-02 0 7141E-01)
19	AUX FW	2	2	5		0	505	0.74595-01	(0.4570E-01 0 1217E+00)
20	PODONI THLECTION DECIDENTION	0	6	A	M	č	603	0.44755-01	(0 1027E-01 0 1949E+00)
20	CHARGING / HIGH- HEAD SAFETY TH JECTION	P	40		M	č	NOG	0.7459E-01	(0.4570F-01.0.1217E+00)
25	CHEMICAL ADDITION (CONTAINMENT SPDAY	1P	5	C	M	č	C10	0.5800E-02	(0.4888E-03.0.6882E-01)
20	COMPONENT-COOLING WATER	P	5	Å	M	č	WOR	0.3135E-01	(0.1905E-01.0.5158E-01)
25	DIESEL-GENERATOR FUEL DIL TRANSFER	P	0	ŝ	M	PD	FO4	0.5120E-02	(0.1067E-02.0.2458E-01)
26	DIESEL-GENERATOR OIL CIRCULATION	P	2	ŝ	M	PD	EO4	0.5120E-02	(0.1067E-02.0.2458E-01)
27	FILTERED SEAL WATER	P	2	A	M	C	WO4	0.3135E-01	(0.1905E-01.0.5158E-01)
28	FIRE	P	2	S	M	PD	X02	0.1955E-01	(0.6145E-02,0.6222E-01)
29	FIRE	P	2	5	D	С	X02	0.6457E-01	(0.1338E-01.0.3116E+00)
30	FUEL DIL TRANSFER	P	2	S	M	PD	X02	0.1955E-01	(0.6145E-02.0.6222E-01)
31	LOW-HEAD SAFETY INJECTION	P	2	S	M	C	503	0.4475E-01	(0.1027E-01.0.1949E+00)
32	INSIDE RECIRCULATION SPRAY	P	2	S	M	C	C10	0.5800E-02	(O.4888E-03,0.6882E-01)
33	OUTSIDE RECIRCULATION SPRAY	P	2	S	Μ	C	C10	0.5800E-02	(0.4888E-03,0.6882E-01)
34	QUENCH SPRAY	P	2	S	M	Ç	C10	0.5800E-02	(0.4888E-03,0.6882E-01)
35	RESIDUAL HEAT REMOVAL	P	2	A	M	C	NO8	0.7459E-01	(0.4570E-01,0.1217E+00)
36	SERVICE WATER	P	2	A	M	C	WO4	0.3135E-01	(0.1905E-01.0.5158E-01)
3.7	CONTROL ROD DRIVE	B	3	A	M	C	NO2	0.7459E-01	(0.4570E-01.0.1217E+00)
38	CORE SPRAY	B	3	S	M	C	503	0.4475E-G1	(0.1027E-01.0.1949E+00)
39	ENGINE-DRIVEN FUEL	B	3	S	D	C	EO4	0.1691E-01	(0.3272E-02,0.8737E-01)
40	FIRE	8	30	5	M	0	X02	0.1955E-01	(0.6145E-02.0.6222E-01)
41	HIGH-PRESSURE COULANT INJECTION	8	3	5	-	C	503	0.1414E-01	(0.2800E-02.0.7141E-01)
42	HPUI DUUSIEN	0	3	2		2	503	0.14146-01	(0.2800E-02,0.7141E-01)
4.5	DAW CODI ING WATER	0	20	A		č	W03	0.31255-01	(0.100/E-02,0.2458E-01) (0.1905E-01 0.5158E-01)
45	DAW COOLING WATER PROSTER	0	20	~	M	č	WOG	0.21255-01	(0.1905E-01 0 5158E-01)
45	PEACTOR BUILDING CLOSED CODI ING	ê	20	Ä	M	č	WO3	0.31355-01	(0.1905E-01 0.5158E-01)
17	PEACTOR CORE ISOLATION COOLING	E	20	ŝ	T	č	501	0 1414E-01	(0 2800F-02 0 7141F-01)
18	RESIDUAL HEAT REMOVAL	B	3	Ă	M	č	NOR	0.74595-01	(0.4570E-01.0.1217E+00)
19	RHR SERVICE WATER	R	3	A	M	č	WO4	0.3135E-01	(0.1905E-01.0.5158E-01)
50	SEAL WATER INJECTION TO FW	B	3	4	M	c	POS	0.2705E-02	(0.8181E-04.0.8941E-01)
5.1	LIQUID CONTROL	B	3	S	M	PD	NO5	0.7459E-01	(0.4570E-01.0.1217E+00)
52	TRANSFER	B	3	S	M	C	EO4	0.5120E-02	(0.1067E-02.0.2458E-01)
53	CONTAINMENT SPRAY	B	4	S	M	C	C10	0.5800E-02	(0.4888E-03.0.6882E-01)
54	CONTROL ROD DRIVE	B	4	A	M	C	NO2	0.7459E-01	(0.4570E-01.0.1217E+00)
55	CORE SPRAY	B	4	S	M	C	503	0.4475E-01	(0.1027E-01.0.1949E+00)
56	CORE SPRAY BOOSTER	B	4	S	M	C	503	0.4475E-01	(0.1027E-01.0.1949E+00)
57	DIESEL-GENERATOR TRANSFER	B	4	S	D	C	EO4	0.1691E-01	(0.3272E-02.0.8737E-01)
8	EMER DIESEL-GENERATOR FUEL	8	4	S	D	PD	EO4	0.1691E-01	(0.3272E-02.0.8737E-01)
59	EMER SERVICE WATER	В	4	S	М	C	WO4	0.3135E-01	(0.1905E-01.0.5158E-01)
50	FIRE	B	4	S	D	C	XO2	0.6457E-01	(0.1338E-01,0.3116E+00)
51	FIRE JOCKEY	В	4	5	M	C	X02	0.1955E-01	(0.6145E-02.0.6222E-01)
12	REACTOR BUILDING CLOSED COOLING	B	4	4	M	C	WO3	0.3135E-01	(0.1905E-01,0.5158E-01)
3	RESIDUAL HEAT REMOVAL	E	4	A	М	C	NOS	0.7459E-01	(0.4570E-01.0.1217E+00)
64	SERVICE WATER	В	4	A	М	C	WO4	0.3135E-01	(0.1905E-01,0.5158E-01)
5	LIQUID CONTROL (POISON)	B	4	S	M	PD	NO5	0.7459E-01	(0.4570E-01.0.1217E+00)

TABLE XV

INCIPIENT DEMAND-RELATED FRAC PUMP FAILURE RATE ESTIMATES PER DEMAND

1	AUX FW	12	1	S	D.	C	\$05	0.1032E+00	(0.6629E-01.0.1606E+00)
2	AUX FW	P		S	Ť.	C	505	0 1032E+00	(0.6629E-01.0.1606E+00)
3	BORIC ACID TRANSFER	P	1	A.	M	C	NOG	0 1438E+00	(0 1030E+00 0 2008E+00)
4	BORON INJECTION RECIRCULATION	P		A	M	C	NOG	0.1438E+00	(0.1030E+00.0.2008E+00)
5	CENTRIFUGAL CHARGING	P		S	M	č	NOG	0 1438E+00	(0.1030E+00.0.2008E+00)
6	COMPONENT-COOLING WATER	P		Ă	M	č	WOR	0.13175+00	(0.9143E-01.0.1897E+00)
7	CONTAINMENT SPRAV		4	0	M	č	C10	0.10116-04	(0 14285-01 0 11425+00)
	DIECEL EHEL DIL TRANCEED	5	1	2	141	~	End	0.40416-01	(0. F220E-02 0. 7748E-01)
0	ETDE	5	1	0	191	5	EO4	0.20326-01	10.53302-02.0.77482-017
10	FIRE CIDE	1	-2.	3	M	C	X02	0.25476+00	10.15932+00.0.40722+00)
10	FIRE IDONEY	2	- 31	2	0	C	X02	0.25476+00	10,15932+00,0.40722+007
11	FIRE DUCKET	2	- 1	S	M	C	X02	0.2547E+00	(0.15932+00.0.40722+00)
12	FW TURBINE EMER LUBE DIL	P	1	S	M	PD	P05	0.2119E-01	(0.3790E-02.0.1185E+00)
13	FW TURBINE LUBE OIL TRANSFER	P	1	S	M	PD	PO5	0.2119E-01	(0.3790E-02.0.1185E+00)
14	RESIDUAL HEAT REMOVAL	P	1	A	M	C	NOB	0.1438E+00	(0.1030E+00.0.2008E+00)
15	SAFETY INJECTION	P	1	S	M	C	503	0.1032E+00	(0.6629E-01,0.1606E+00)
16	SERVICE WATER	P	1	A	M	C	WO4	0.1317E+00	(0.9143E-01.0.1897E+00)
17	SERVICE WATER BODSTER	P	1	Α	M	C	W04	0.1317E+00	(0.9143E-01,0.1897E+00)
18	AUX FW	P	2	S	M	C	S05	0.1032E+00	(0.6629E-01.0.1606E+00)
19	AUX FW	P	2	S	T	C	S05	0.1032E+00	(0.6629E-01.0.1606E+00)
20	BORIC ACID TRANSFER	P	2	A	M	C	N09	0.1438E+00	(0.1030E+00.0.2008E+00)
21	BORON INJECTION RECIRCULATION	P	2	A	M	C	503	0.1032E+00	(0.6629E-01.0.1606E+00)
22	CHARGING/HIGH-HEAD SAFETY INJECTION	P	2	A	M	C	NO9	0.1438E+00	(0.1030E+00.0.2008E+00)
23	CHEMICAL ADDITION (CONTAINMENT SPRAY)P	2	S	M	C	C10	0.4041E-01	(0.1428E-01.0.1143E+00)
24	COMPONENT-COOLING WATER	P	2	Ä	M	C	WO3	0.1317E+00	(0.9143E-01.0.;897E+00)
25	DIESEL-GENERATOR FUEL OIL TRANSFER	P	2	S	M	PD	EQ4	0 2032E-01	(0.5330E-02.0.7748E-01)
26	DIESEL-GENERATOR OIL CIRCULATION	P	2	č	M	PD	EQ4	0 20328-01	(0.5330E-02.0.7748E-01)
27	FILTERED SEAL WATER	P	2	Ă	M	0	WOA	0 13175+00	(0 9143E-01 0 1897E+00)
28	FIRE	D	5	ŝ	M	PD	XO2	0.15176+00	(0 1593E+00 0 4073E+00)
29	FIDE	D	5	č	5	2	XOD	0.25476+00	(0.15932+00.0.40722+00)
30	FIFE OTL TRANSFER	0	5	0	N.	DO	XOZ	0.25476+00	10.15932+00.0.40722+00)
24	IOW-HEAD SAFETY THUECTION	0	-	0		PU	602	0.25476400	(0.15932+00.0.40722+00)
35	THISTOP DECTOCILLATION CODAY	P	40	2	M	č	503	0.10328+00	(0.66292-01.0.16062+00)
32	DUTCIDE DECIDEULATION SPRAT	5	-	2	PV1	0	010	0.40412-01	(0.1428E-01.0.1143E+00)
33	OUTSIDE RECIRCULATION SPRAT	2	4	3	M	C	C10	0.40418-01	(0.1428E-01.0.1143E+00)
34	QUENCH SPRAT	P	2	3	M	C	C10	0.4041E-01	(0.1428E-01,0.1143E+00)
30	RESIDUAL MEAT REMOVAL	2	2	A	M	C	NOS	0.1438E+00	(0.1030E+00.0.2008E+00)
30	SERVICE WATER	P	2	A	M	C	W04	0.1317E+00	(0.9143E-01.0.1897E+00)
37	CONTROL ROD DRIVE	B	3	A	M	C	NO2	0.4942E-01	(0.3356E-01,0.7278E-01)
38	CORE SPRAY	8	3	S	M	C	503	0.35468-01	(0.2199E-01,0.5718E-01)
38	ENGINE-DRIVEN FUEL	B	3	S	D	C	EO4	0.6985E-02	(0.1881E-02,0.2594E-01)
40	FIRE	B	3	S	Μ	C	X02	0.8753E-01	(0.5165E-01,0.1483E+00)
41	HIGH-PRESSURE COOLANT INJECTION	B	3	S	Т	C	S03	0.3546E-01	(0.2199E-01,0.5718E-01)
42	HPCI BOOSTER	B	3	S	T	C	503	0.3546E-01	(0.2199E-01.0.5718E-01)
43	LUBE OIL TRANSFER	B	3	S	M	C	EO4	0.6985E-02	(0.1881E-02.0.2594E-01)
44	RAW COOLING WATER	B	3	A	M	C	WO3	0.4526E-01	(0.3326E-01.0.6160E-01)
45	RAW COOLING WATER BODSTER	B	3	A	Μ	C	WO3	0.4526E-01	(0.3326E-01.0.6160E-01)
46	REACTOR BUILDING CLOSED COOLING	B	3	A	M	C	WO3	0.4526E-01	(0.3326E-01.0.6160E-01)
47	REACTOR CORE ISOLATION COOLING	B	3	S	T	C	501	0.3546E-01	(0.2199E-01.0.5718E-01)
48	RESIDUAL HEAT REMOVAL	8	3	A	M	C	NO8	0.4942E-01	(0.3356E-01.0.7278E-01)
49	RHR SERVICE WATER	B	3	A	M	C	WO4	0.45268-01	(0.3326E-01.0.6160E-01)
50	SEAL WATER INJECTION TO FW	B	3	A	M	c	POS	0 72855-02	(0 1321E-02 0 4016E-01)
51	LIQUID CONTROL	R	3	5	M	PD	NOS	0 49425-01	(0.3356E-01 0.7278E-01)
52	TRANSFER	R	3	ŝ	M	C	FOA	0 69855-00	(0.1884E-02 0.2504E-01)
53	CONTAINMENT SPRAY	R	4	é	M	č	C10	0.00000002	(0.1801E-02.0.2094E-01)
54	CONTROL ROD DRIVE	Ē	4	Å	M	č	NOD	0.10000-01	(0.4718E-02.0.4083E-01)
E.E.	CODE SDDAV	0	7	C		2	602	0.49426-01	10.33562-01.0.72782-01
50	CODE EDDAV DODETED	0	4	2	M	6	503	0.3546E-01	(0.2199E-01,0.5718E-01)
50	OURE SPRAT DUUSIER	0	4	2	M	C	503	0.35462-01	(0.2199E-01,0.5718E-01)
0/	ENER DIFFEL OFNERATOR FUEL	B	4	2	0	C	E04	0.69858-02	(0.1881E-02,0.2594E-01)
80	EMER DIESEL GENERATOR FUEL	B	4	S	0	PD	E04	0.6985E-02	(0.1881E-02.0.2594E-01)
09	EMER SERVICE WATER	B	4	S	M	Ç	W04	0.4526E-01	(0.3326E-01,0.6160E-01)
00	FIRE	B	4	S	D	C	X02	0.8753E-01	(0.5165E-01,0.1483E+00)
61	FIRE JOCKEY	B	4	S	M	C	X02	0.8753E-01	(0.5165E-01,0.1483E+00)
62	REACTOR BUILDING CLOSED COOLING	В	4	Α	M	C	WO3	0.4526E-01	(0.3326E-01,0.6160E-01)
63	RESIDUAL HEAT REMOVAL	B	4	A	M	C	NO8	0.4942E-01	(0.3356E-01,0.7278E-01)
64	SERVICE WATER	B	4	A	M	C	WO4	0.4526E-01	(0.3326E-01.0.6160E-01)
65	LIQUID CONTROL (POISON)	B	4	S	M	PD	NO5	0.4942E-01	(0.3356E-01.0.7278E-01)

TABLE XVI

CATASTROPHIC TIME-DEPENDENT FRAC PUMP FAILURE RATE ESTIMATES PER OPERATING HOUR

1	CODIC LOID TRANSFER	5			8.4	r .	NOO	0 96455-04	(0 4440E-04 0 2095E-03)
1	BURIC ACID TRANSFER	5	1	~	10	~	NOG	0.96455-04	(0 4440E-04 0 2095E-03)
2	BORDN INJECTION RECIRCULATION	1			141 8.6	č	DOG	0.96456-04	(0 4440E-04 0 2095E-03)
3	CIRCULATING WATER	2	1	R	M	5	MOD	0.90405-04	(0.4440E-04,0.2005E-03)
4	COMPONENT - COOLING WATER	H	3.	A	M	0	WUS	0.90456-04	(0.4440E-04,0.2000E-02)
5	CONDENSATE	P	1	R	M	C	P04	0.96451-04	10.44402-04.0.20952-031
6	FW TURBINE MAIN LUBE DIL	P	1	R	M	PD	P05	0.9645E-04	10.44402-04.0.20952-031
7	CHARGING	P	1	R	M	PD	NO9	0.9645E-04	(0.4440E-04,0.2095E-03)
8	REACTOR COOLANT	P	1	R	M	C	NO4	0.9645E-04	(0.4440E-04.0.2095E-03)
9	RESIDUAL HEAT REMOVAL	P	1	A	M	C	NO8	0.9645E-04	(0.4440E-04.0.2095E-03)
10	SERVICE WATER	P	1	A	M	C	W04	0.9645E-04	(0.4440E-04,0.2095E-03)
11	SERVICE WATER BOOSTER	P	1	A	M	C	W04	0.9645E-04	(0.4440E-04.0.2095E-03)
12	STEAM GENERATOR FEED	P	1	R	T	C	PO5	0.3803E-03	(0.1539E-03,0.9398E-03)
13	BORIC ACID TRANSFER	p	2	A	M	C	NO9	0.9645E-04	(0.4440E-04,0.2095E-03)
14	BORON INJECTION RECIRCULATION	p	2	A	M	C	503	0.9645E-04	(0.4440E-04,0.2095E-03)
15	CHARGING/HIGH-HEAD SAFETY INJECTION	p	2	A	M	C	NO9	0.9645E-04	(0.4440E-04.0.2095E-03)
16	CIDCULATING WATER	P	2	R	M	C	P06	0.9645E-04	(0.4440E-04.0.2095E-03)
17	COMPONENT-COOLING WATER	P	5	4	M	C	WO3	0.96455-04	(0.4440E-04.0.2095E-03)
10	CONDENSATE	p ·	5	P	M	c	PO4	0.9645E-04	(0.4440E-04.0.2095E-03)
10	ETI TEDEN CENI WATED	P	3	A	M	č	WO4	0.9645E-04	(0.4440E-04.0.2095E-03)
20	DEACTOD COOLANT	P	2	p	M	č	NO4	0.9645E-04	(0.4440E-04.0.2095E-03)
20	DESTDUAL WEAT DEMOVAL	P	0	A	M	č	NOS	0.9645E-04	(0.4440E-04.0.2095E-03)
00	CEDUICE WATED	D	5	~	M	č	WOA	0.96455-04	(0.4440E-04.0.2095E-03)
44	SERVICE WATER	D	5	p	M	č	POS	0 96455-04	(0.4440F-04.0.2095E-03)
23	STEAM GENERATUR FEED		- 2	D	24	č	POU	0.00995-04	(0.9337E-05.0.4672E-04)
24	CONDENSATE	0	0	R	P.1	~	004	0.20096-04	(0 9227E-05 0 4672E-04)
25	CONDENSATE BUDSTER	0	5	R D	PV1	5	POA	0.20096-04	(0.9337E-05.0.4672E-04)
26	CONDENSER CIRCULATING	D	00	ĸ	101	0	NOO	0.20092-04	(0.9337E-05 0 4672E-04)
27	CONTROL ROD DRIVE	B	00	A	Nº.	č	NO2	0.20896-04	(0.9337E-05.0.4672E-04)
28	RAW COOLING WATER	5	0		105	5	WOS	0.20892-04	(0.9337E-05.0.4672E-04)
29	RAW COOLING WATER BOOSTER	B	3	A	M	0	WO3	0.2089E-04	(0.9337E-05.0.4672E-04)
30	REACTOR BUILDING CLOSED COOLING	Б	3	A	M	C	WO3	0.20898-04	10.93376-05.0.46726-047
31	REACTOR FW	B	3	R	1	C	P05	0.82346-04	(0.3361E-04.0.2017E-037
32	REACTOR RECIRCULATING	В	3	R	M	C	NO4	0.20891-04	10.93376- 5.0.46725-047
33	RESIDUAL HEAT REMOVAL	B	3	A	M	C	80N	0.2089E-04	(0.9337E-05.0.4672E-04)
34	RHR SERVICE WATER	B	3	A	M	C	WO4	0.2089E-04	(0.9337E-05,0.4672E-04)
35	SEAL WATER INJECTION TO FW	E	3	A	M	C	POS	0.2089E-04	(0,9337E-05,0.4672E-04)
36	CIRCULATION	В	4	R	M	C	P06	0.2089E-04	(0.9337E-05,0.4672E-04)
37	CONDENSATE	B	4	R	M	C	P04	0.2089E-04	(0.9337E-05,0.4672E-04)
38	CONTROL ROD DRIVE	E	4	A	M	C	NO2	0.2089E-04	(0.9337E-05,0.4672E-04)
39	REACTOR BUILDING CLOSED COOLING	E	4	Δ	M	C	WO3	0.2089E-04	(0.9337E-05.0.4672E-04)
40	REACTOR FW	B	4	R	M	C	PO5	0.2089E-04	(0.9337E-05.0.4672E-04)
41	REACTOR RECIRCULATING	B	4	R	M	C	NO4	0.2089E-04	(0.9337E-05,0.4672E-04)
42	RESIDUAL HEAT REMOVAL	E	4	A	M	C	NOB	0.2089E-04	(0.9337E-05.0.4672E-04)
43	SERVICE WATER	B	4	A	M	C	WO4	0.2089E-04	(0.9337E-05,0.4672E-04)

TABLE XVII

DEGRADED TIME-DEPENDEN'T FRAC PUMP FAILURE RATE ESTIMATES PER OPERATING HOUR

1	BORIC ACID TRANSFER	P		Δ	M	С	NO9	0.4356E-03	(0.2062E-03.0.9203E-03)
2	BORON INJECTION RECIRCULATION	P	1	A	M	C	NO9	0.4356E-03	(0.2062E-03.0.9203E-03)
3	CIRCULATING WATER	P	1	R	M	C	P06	0.1592E-03	(0.9295E-04.0.2726E-03)
4	COMPONENT-COOLING WATER	P	1.	A	M	C	WO3	0.7349E-04	(0.3480E-04.0.1552E-03)
5	CONDENSATE	P	1	R	M	C	PO4	0.1592E-03	(0.9295E-04.0.2726E-03)
6	FW TURBINE MAIN LUBE OIL	P	1	R	M	PD	POS	0.1592E-03	(0.9295E-04.0.2726E-03)
7	CHARGING	P	1	R	M	PD	NO9	0.8845E-04	(0.3044E-04 0.2571E-03)
8	REACTOR COOLANT	P	1.	R	M	C	NO4	0.8845E-04	(0.3044E-04 0.2571E-03)
9	RESIDUAL HEAT REMOVAL	P	1	A	M	C	NO8	0.4356E-03	(0.2062E-03.0 9203E-03)
10	SERVICE WATER	P	. 1	Δ	M	C	WO4	0.7349E-04	(0.3480E-04 0.1552E-03)
11	SERVICE WATER BODSTER	P	1	A	м	C	W04	0.7349E-04	(0.3480E-04 0 1552E-03)
12	STEAM GENERATOR FEED	P	. 1	R	T	C	PO5	0.1592E-03	(0.9295E-04.0.2726E-03)
13	BORIC ACID TRANSFER	p	2	A	M	C	NO9	0.4356E-03	(0.2062E-03.0.9203E-03)
14	BORON INJECTION RECIRCULATION	P	2	A	M	C	\$03	0.2381E-04	(0.4078E-07.0.1390E-01)
15	CHARGING/HIGH-HEAD SAFETY INJECTION	P	2	A	M	C	NO9	0.4356E-03	(0.2062E-03.0.9203E-03)
16	CIRCULATING WATER	P	2	R	M	C	POG	0.15921-03	(0.9295E-04.0.2726E-03)
17	COMPONENT-COOLING WATER	P	2	A	M	C	WO3	0.7349E-04	(0.3480E-04 0 1552E-03)
18	CONDENSATE	P.	2	R	M	C	PO4	0.1592E-03	(0.9295E-04 0.2726E-03)
19	FILTERED SEAL WATER	P	2	A	M	C	WO4	0.7349E-04	(0.3480E-04.0.1552E-03)
20	REACTOR CODLANT	P	2	R	M	C	NO4	0.8845E-04	(0.3044E-04 0.2571E-03)
21	RESIDUAL HEAT REMOVAL	P	2	Δ	M	C	NO8	0.4356E-03	(0.2062E-03.0.9203E-03)
22	SERVICE WATER	P	2	A	M	C	WO4	0.7349E-04	(0.3480E-04.0.1552E-03)
23	STEAM GENERATOR FEED	P	2	R	M	C	POS	0.1592E-03	(0.9295E-04 0.2726E-03)
24	CONDENSATE	B	3	R	M	C	PO4	0.7084E-04	(0.3934E-04 0 1276E-03)
25	CONDENSATE BOOSTER	B	3	R	M	C	PO4	0.7084E-04	(0.3934E-04.0.1276E-03)
26	CONDENSER CIRCULATING	B	3	R	M	C	P06	0.7084E-04	(0.3934E-04.0.1276E-03)
27	CONTROL ROD DRIVE	B	3	A	M	C	NO2	0.1939E-03	(0, 1112E-03, 0, 3382E-03)
28	RAW COOLING WATER	B	3	A	M	C	WO3	0.3271E-04	(0.1539E-04.0.6949E-04)
29	RAW COOLING WATER BOOSTER	B	3	A	M	C	WO3	0.3271E-04	(0.1539E-04.0.6949E-04)
30	REACTOR BUILDING CLOSED COOLING	B	3	Α	M	C	WO3	0.3271E-04	(0.1539E-04.0.6949E-04)
31	REACTOR FW	B	3	R	T	C	POS	0.7084E-04	(0.3934E-04.0.1276E-03)
32	REACTOR RECIRCULATING	B	3	R	M	C	NO4	0.3937E-04	(0.1436E-04.0.1079E-03)
33	RESIDUAL HEAT REMOVAL	B	3	A	M	C	NO8	0.1939E-03	(0,1112E-03,0,3382E-03)
34	RHR SERVICE WATER	B	3	A	M	C	WO4	0.3271E-04	(0.1539E-04.0.6949E-04)
35	SEAL WATER INJECTION TO FW	8	3	A	M	C	POS	0.3489E-03	(0.1018E-03.0.1195E-02)
36	CIRCULATION	B	4	R	M	C	P06	0.7084E-04	(0.3934E-04.0.1276E-03)
37	CONDENSATE	E	4	R	M	C	PO4	0.7084E-04	(0.3934F-04 0 1276E-03)
38	CONTROL ROD DRIVE	E	4	A	M	C	NO2	0.1939E-03	(0.1112E-03.0.3382E-03)
39	REACTOR BUILDING CLOSED COOLING	B	4	A	M	C	W03	0.3271E-04	(0.1539E-04.0.6949E-04)
40	REACTOR FW	B	4	R	M	C	POS	0.7084E-04	(0.3934E-04.0.1276E-03)
41	REACTOR RECIRCULATING	B	4	R	M	C	NO4	0.3937E-04	(0.1436E-04.0.1079E-03)
42	RESIDUAL HEAT REMOVAL	B	4	A	M	C	NOS	0.1939E-03	(0.1112E-03.0.3382E-03)
43	SERVICE WATER	B	4	A	M	C	WO4	0.3271E-04	(0, 1539E-04, 0, 6949E-04)
							and the second se		

TABLE XVIII

INCIPIENT TIME-DEPENDENT FRAC PUMP FAILURE RATE ESTIMATES PER OPERATING HOUR

				1.0		1.0			
1	BORIC ACID TRANSFER	P	1	A	M	C	NOS	0.45251-03	(0.3413E-03,0.5999E-03)
2	BORON INJECTION RECIRCULATION	P	1	A	M	C	NO9	0.4525E-03	(0.3413E-03,0.5999E-03)
3	CIRCULATING WATER	P	1	R	M	C	P06	0.4525E-03	(0.3413E-03,0.5999E-03)
4	COMPONENT-COOLING WATER	P	1	A	M	C	WO3	0.4525E-03	(0.3413E-03,0.5999E-03)
5	CONDENSATE	P	.t.	R	M	C	PO4	0.4525E-J3	(0.3413E-03,0.5999E-03)
6	FW TURBINE MAIN LUBE OIL	P	1	R	M	PD	PO5	0.4525E-03	(0.3413E-03.0.5999E-03)
7	CHARGING	P	1.	R	M	PD	NO9	0.4525E-03	(0.3413E-03,0.5999E-03)
8	REACTOR CODLANT	P	1	R	M	C	NO4	0.4525E-03	(0.3413E-03,0.5999E-03)
9	RESIDUAL HEAT REMOVAL	P	1	A	M	С	NO8	0.4525E-03	(0.3413E-03,0.5999E-03)
10	SERVICE WATER	P	1	A	M	C	WO4	0.4525E-03	(0.3413E-03,0.5999E-03)
11	SERVICE WATER BOOSTER	P	1	A	M	C	WO4	0.4525E-03	(0.3413E-03.0.5999E-03)
12	STEAM GENERATOR FEED	P	1	R	T	C	PO5	0.9769E-03	(0.5874E-03.0.1625E-02)
13	RODIC ACTO TRANSFER	P	2	4	M	C	N09	0.4525E-03	(0.3413E-03.0.5999E-03)
14	RODON INJECTION DECIDCULATION	P	2	4	M	č	503	0.4525E-03	(0.3413E-03.0.5999E-03)
15	CHARCING HIGH-HEAD SAFETY INJECTION	P	2	A	M	č	NO9	0.4525E-03	(0.3413E-03.0.5999E-03)
16	CIDCHLATING WATED	P	5	D.	M	č	POG	C. 4525E-03	(0.3413E-03.0.5999E-03)
10	COMPONENT COOL THE WATER	p	5	A	M	č	WO3	0.4525E-03	(0.3413E-03.0 5999E-03)
+0	COMPONENT COULING WATER	6	2	6	M	č	PO4	0 45258-03	(0.3413F-03.0.5999E-03)
10	ETITEDED CEAL WATED	0	5	2	M	č	WOA	0 4525E-03	(0.3413E-03.0.5999E-03)
19	DEACTOD CODIANT	P	5	p	M	č	NO4	0 45255-03	(0.3413E-03.0.5999E-03)
20	DESTENIAL HEAT DEMOVAL	6	5	~	5.8	č	NOR	0 45255-03	(0 3413E-03 0 5999E-03)
21	CEDUICE WATED	0	-	~		č	WO4	0 45255-03	(0 3413E-03 0 5999E-03)
44	STEAN OFNEDATED FFED	P	5	D	M	č	POS	0 45255-03	(0 3413E-03 0 5999E-03)
23	STEAM GENERATUR FEED	P	40	D	M	č	POA	0.43236-03	(0, 1020E-03, 0, 1825E-03)
24	CUNDENSATE DOOGTED	0	2	P	14	č	POA	0.13645-03	(0.1020E-03.0.1825E-03)
20	CONDENSATE BUUSTER	P	20	0	82	č	POA	0.13646-03	(0 1020E-03 0 1825E-03)
20	CUNDENSER CIRCULATING	0	00		84	č	NOO	0.13645-03	(0 10205-03 0 18255-03)
21	CUNTRUL RUD DRIVE	0	20	~	M	č	WO2	0 10645-00	(0.10205-02.0.18255-02)
28	RAW COULING WATER DOOCTED	5	20	~	A.	20	WOR	0.13646-03	(0.1020E-03,0.1825E-03)
29	RAW GOULING WATER BUDSTER	0	0			2	WOO	0.13646-03	(0.10206-03.0.18256-03)
30	REACTOR BUILDING CLUSED COULING	D	3		T	č	POS	0.13046-03	(0. 1020E-03,0. 1025E-03)
31	REACTOR FW	0	00	D		5	NOA	0.29402-03	(0.1037E-03.0.102E-03)
32	REACTOR REC'RCULATING	D	3	ĸ	111	~	NOA	0.13646-03	(0.10206-03.0.18256-03)
33	RESIDUAL HEAT REMOVAL	B	0	A	PM .	0	NOA	0.13642-03	(0,10206-03,0,18256-03)
34	RHR SERVICE WATER	B	3	A	M	0	WO4	0.1304E-03	(0.10206-03.0.18256-03)
35	SEAL WATER INJECTION TO FW	B	3	A	M	0	PUD	0.1334E-03	(0.10202-03.0.18252-03)
36	CIRCULATION	В	4	R	M	C	P06	0.1364E-03	(0.1020E-03.0.1825E-03)
37	CONDENSATE	B	4	R	M	Ç	P04	0.1364E-03	(0.1020E-03.0.1825E-03)
38	CONTROL ROD DRIVE	В	4	A	M	C	NO2	0.1364E-03	(0.1020E-03.0.1825E-03)
39	REACTOR BUILDING CLOSED COOLING	B	4	A	M	C	WO3	0.1364E-03	(0.1020E-03,0.1825E-03)
40	REACTOR FW	B	4	R	M	C	PO5	0.1364E-03	(0.1020E-03.0.1825E-03)
41	REACTOR RECIRCULATING	B	4	R	M	C	N04	0.1364E-03	(0.1020E-03.0.1825E-03)
42	RESIDUAL HEAT REMOVAL	B	4	A	M	C	NO8	0.1364E-03	(0.1020E-03.0.1825E-03)
43	SERVICE WATER	В	4	A	M	C	WO4	0.1364E-03	(0.1020E-03.0.1825E-03)

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APPENDIX A

CODED IPRDS PUMP FAILURE DATA BASES

TABLE A-I

DESCRIPTION OF THE DEMAND-RELATED FAILURE DATA BASE

Factors	Columns
RTYPE (Reactor Type)	(2)
PWR	1
BWR	2
SYSTEM	(4)
Nuclear	1
Engineered Safety	2
Containment	3
Electrical	4
Power Conversion	5
Process Auxiliary	6
Plant Auxiliary	7
PLANT	(43)
Plant 1 (PWR)	1
Plant 2 (PWR)	2
Plant 3 (RWR)	2
Plant 4 (BWR)	4
OPMODE (Operating Mode)	(45)
Standby	1
Alternating	2
PTYPE (Pump Type)	(47)
Positive Displacement	1
Centrifugal	2
DRIVER	(49)
Motor	1
Diesel	2
Turbine	3
Number of Catastrophic Demand-Related Failures	(50-54)
Number of Degraded Demand-Related Failures	(55-59)
Number of Incipient Demand-Related Failures	(60-65)
Population Demands ^a	(66-74)

^aTotal number of component demands in the operating period.

TABLE A-II

									100 C
1	2	AUX FW	1	1 2	2	1	14	12	60
1	2	AUX FW	1	1 2	3		2	7	60
1	1	BORIC ACID TRANSFER	1	2 2	1	2	1	11	120
1	1	BORON INJECTION RECIRCULATION	1	2 2	1	0	3	34	120
4	4	CENTRIFUGAL CHARGING	1	1 2	1	4	1	19	120
1	-	COMPONENT CONTINUE WATED	÷.	0 0	÷	0	0	15	180
3	0	COMPONENT CODAY	4	1 5	-	4	õ	7	120
3	3	CUNTAINMENT SPRAY	1	1 4			~	0	+20
3	4	DIESEL FUEL DIL TRANSFER	1	1 4	1	2	~	-	60
1	7	FIRE	1	1 4	1	÷	4	1	60
1	7	FIRE	-1	1 2	2	1	- 1	4	60
1	7	FIRE JOCKEY	1	1 2	1	0	1	29	60
1	5	FW TURBINE EMER LUBE OIL	1	1 1	1	0	0	1	120
1	5	FW TURBINE LUBE OIL TRANSFER	1	1 1	1	0	0	0	60
1	1	RESIDUAL HEAT REMOVAL	1	2 2	1	3	0	13	120
1	2	SAFETY INJECTION	1	1 2	1	1	0	14	120
÷.	6	SERVICE WATER	1	2 2	1	0	6	16	180
	6	SERVICE WATER BOOSTER		2 2	1	1	6	20	240
-	5	ANY EW	5	1 2	1	0	1	3	38
4	-	AUX EW	5	1 2	8	õ	0	4	19
- 2	-	BODIC ACTO TRANSFER	5	2 2	4	õ	õ	0	38
1	1.2	BURIC ACTU IRANOFER	4 0	6 6	-	õ	õ	4	38
1	2	BURUN INJECTION RECIRCULATION	4	4 4	1	0	~	7	50
- 3	- 1	CHARGING/HIGH-HEAD SAFELY INJECTION	4	4 4	1	-	4		10
1	3	CHEMICAL ADDITION (CONTAINMENT SPRAY	12	1 2	1	1	0	1	19
1	6	COMPONENT-COOLING WATER	2	2 2	1	0	0	0	58
1	4	DIESEL-GENERATOR FUEL OIL TRANSFER	2	1 1	1	0	2	0	11
1	-4	DIESEL-GENERATOR OIL CIRCULATION	2	1 1	1	0	0	1	38
1	6	FILTERED SEAL WATER	2	2 2	1	0	0	0	38
1	7	FIRE	2	1 1	1	1 t.	1	2	19
1	7	FIRE	2	1 2	2	5	0	1	19
1	7	FUEL OIL TRANSFER	2	1.1	1	0	0	0	19
1	2	IOW-HEAD SAFETY INJECTION	2	1 2	4	0	0	0	38
-	3	INSTOR RECIRCULATION SPRAY	2	1 2	1	0	0	0	38
4	3	DUTSIDE DECIDCULATION SPRAY	3	1 2	1	0	ö	õ	38
12	20	OUENCE CODAV	5	1 2	÷.	õ	õ	1	38
- 2	0	DECTOUR HEAT DEMOVAL	- 0	0 0	÷.	0	õ		38
1	1	REDIDUAL MEAT REMUVAL	10	6 6 0		ŏ	0		50
12	0	SERVICE WATER	4	2 2	1		24		210
2	1	CONTROL ROD DRIVE	3	2 2	. 1	1	34	9	210
2	2	CORE SPRAY	3	1 2	1	0	0	4	520
2	4	ENGINE-DRIVEN FUEL	3	1 2	2	0	0	0	520
2	7	FIRE	3	1 2	1	6	1	2	170
-2	2	HIGH-PRESSURE COOLANT INJECTION	3	1 2	3	4	1	3	130
2	2	HPCI BOOSTER	3	1 2	3	0	0	5	130
2	4	LUBE OIL TRANSFER	3	1 2	1	1	0	1	56
2	6	RAW COOLING WATER	3	2 2	1	3	1	16	520
0	6	RAW COOLING WATER BOOSTER	3	2 2	1	0	1	14	184
1	6	REACTOR BUILDING CLOSED COOLING	3	2 2	1	0	1	6	390
- 5	2	REACTOR CORE ISOLATION COOLING	3	1 2	3	0	1	0	130
	1 4	RESTDUAL HEAT REMOVAL	3	2 2	4	2	2	7	520
-		PHP SERVICE WATER	5	2 2		2	9	43	430
		SEAL WATED INJECTION TO EW	-	0 0	4	0	0	3	260
1		LITOUTO CONTROL				2	4	11	260
		TRANSFER				2	~		960
	6 4	I TRANSFER	3			2	0	2	200
	2 3	CUNTAINMENT SPRAY	1		1.10	-	0	-	200
	1	CONTROL ROD DRIVE	. *		1	1	0	8	144
	2 2	CORE SPRAY	. 4	1 3	1	1	0	10	288
-	2 2	CORE SPRAY BOOSTER		1 1 2	1	0	0	4	288
1	2 4	DIESEL-GENERATOR TRANSFER	. 6	1 1 2	2	0	0	0	287
1	2 4	EMER DIESEL-GENERATOR FUEL	4	1 1 1	2	0	2	3	144
1	2 6	5 EMER SERVICE WATER		1 1 2	1	6	20	11	288
1	2 7	7 FIRE		1 1 2	2 2	2	1	14	144
	2 4	FIRE JUCKEY		1 1 2	2 1	0	0	0	72
1	2 6	REACTOR BUILDING CLOSED COOLING		1 2 3	2 1	0	0	6	144
	3	RESTOUAL HEAT REMOVAL		1 2	2 1	õ	õ	2	216
	5 1	SERVICE WATER		1 2 1	2 1	1	2	7	144
	3	LITOUTO CONTROL (DOTSON)		4 4		n.	õ	0	144
	6	I FIGOID CONTROL (FOIDON)				~	N.	0	144

THE CODED PUMP DEMAND-RELATED FAILURE DATA BASE

2

TABLE A-III

Factors	Columns
RTYPE (Reactor Type)	(2)
PWR	1
BWR	2
SYSTEM	(4)
Nuclear	1
Engineered Safety	2
Power Conversion	3
Process Auxiliary	4
PLANT	(43)
Plant 1 (PWR)	1
Plant 2 (PWR)	2
Plant 3 (BWR)	3
Plant 4 (BWR)	4
OPMODE (Operating Mode)	(45)
Running	1
Alternating	2
PTYPE (Pump Type)	(47)
Positive Displacement	1
Centrifugal	2
DRIVER	(49)
Motor	1
Turbine	2
Number of Catastrophic Time-Dependent Failures	(50-54)
Number of Degraded Time-Dependent Failures	(55-59)
Number of Incipient Time-Dependent Failures	(60-65)
Population Hours ^a	(66-74)

-

DESCRIPTION OF THE TIME-DEPENDENT FAILURE DATA BASE

^aTotal number of component hours (in the operating mode) in the operating period.

TABLE A-IV

THE CODED FUMP TIME-RELATED FAILURE DATA BASE

	+	BORIC ACID TRANSFER	1	2	2	1	0	1	1.1	44000
		BORON INJECTION RECIRCULATION	1	2	2	1	0	3	34	44000
	2	CIDCULATING WATER	1	1	2	1	5	4	23	48400
1	4	COMPONENT COOL THE WATER	1	2	2		1	0	15	44000
1	-	COMPONENT COOLING WATCH		-	5		3	5	18	48000
3	3	CUNUENSAIE MATH LUDE OT		-	-	4	ő		1	48000
-39	3	FW TURBINE MAIN LUDE OIL		-		-			25	24000
1	1	CHARGING	1	2		1		~	20	24000
1	-1	REACTOR CODLANT	1	-	6	1		0	40	20000
1	1	RESIDUAL MEAT REMOVAL	1	4	4	1	-	č	15	20000
1	4	SERVICE WATER	1	*	4	2	3	0	10	19000
1	4	SERVICE WATER BOOSTER	1	2	2	1	5	6	20	110000
1	3	STEAM GENERATOR FEED	1	1	2	2	8	11	29	48000
1.	1	PORIC ACID TRANSFER	2	2	2	1	0	0	0	14000
1	2	BORON INJECTION RECIRCULATION	2	2	2	1	4	0	4	14000
1	1	CHARGING HIGH-HEAD SAFETY INJECTION	2	2	2	1	2	4	7	6500
1	3	CIRCULATING WATER	2	1	2	1	3	3	18	25800
1	4	COMPONENT COOLING WATER	2	2	2	1	0	0	0	14000
1	3	CONDENSATE	2	1	2	1	3	10	4	13000
1	4	FILTERED SEAL WATER	2	2	2	1	0	0	0	14000
1	1	REACTOR COOLANT	2	1	2	1	0	0	1	19320
1	1	RESIDUAL HEAT REMOVAL	2	2	2	1	0	0	1	7600
1	4	SERVICE WATER	2	2	2	1	3	2	4	25000
1	3	STEAM GENERATOR FEED	2	1	2	1	6	2	8	13000
2	3	CONDENSATE	3	1	2	1	0	1	9	160000
2	3	CONDENSATE BOOSTER	3	1	2	1	0	6	33	160000
2	3	CONDENSER CIRCULATING	3	1	2	1	2	5	6	160000
5	4	CONTROL ROD DRIVE	3	2	2		3	34	9	110000
3	â	RAW COOLING WATER	3	2	2	1	4	1	16	230000
3	4	RAW COOLING WATER BOOSTER	3	2	2	1	0	1.1	14	82000
5	4	PEACTOR BUILDING CLOSED COOLING	12	2	2	1	õ	1	6	95000
5	-	DEACTOR FW	3	1	2	2	13	14	30	160000
2	4	PEACTOR RECTROULATING	3	÷	5	1	0	4	13	110000
10	-	RESTOLAL HEAT REMOVAL	3	2	2	+	1	2	7	42000
5		DUD SEDVICE WATED	3	2	5		3	ā	43	110000
1	2	CEAL WATED IN FOTION TO FW	3	5	0	- 6	1	õ	3	54000
-	3	STAL WATER INVECTION TO TH	4	-	0			õ	6	150000
-	3	CONDENCATE	A	4	5			õ	4	110000
4	3	CONTROL DOD DETVE	-		- 0		2	õ		37000
4	1	DEACTOD BULLISTNC CLOSED COOLING		-	5		ő	õ	6	52000
4 1	4 0	REACTOR BUILDING SLUSED GOULING	1	-	* 2			0	10	110000
4	3	DEACTOR DECTROUMATING			* 13	-		5	25	187000
4	1	REACTOR RECIRCULATING	-	-	* 0	1	-	0	20	15000
-	1	RESIDUAL MEAT REMUVAL		40	4 5	1		0		84000
2	4	SERVICE WATER	- 4	*	*			4	1	84000

2

1

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APPENDIX B

DEGRADED AND INCIPIENT DEMAND-RELATED PUMP FAILURE RATE ANALYSES

TABLE B-I

DEGRADED DEMAND-RELATED FRAC FAILURE RATE MODEL ANALYSIS

One	-Factor	Models
	RTYPE	
	SYSTEM	
	OPMODE	
	PTYPE	
	DRIVER	

----- 0.1085×10^{-1} 0.6203 0.8493×10^{-1} 0.8888×10^{-1}

P-Values

P-Values

 $\begin{array}{c} 0.9137\\ 0.2035 \times 10^{-1}\\ 0.9021\\ 0.2310\\ 0.1549\\ 0.1473 \times 10^{-1}\\ 0.1687 \times 10^{-1}\\ 0.1687 \times 10^{-2}\\ 0.9448 \times 10^{-1}\\ 0.2313\\ 0.3525 \times 10^{-1}\end{array}$

Two-Factor Models

RTYPE, PLANT
RTYPE, SYSTEM
RTYPE, OPMODE
RTYPE, PTYPE
RTYPE, DRIVER
SYSTEM, OPMODE
SYSTEM, PTYPE
SYSTEM, DRIVER
OPMODE, DRIVER
OPMODE, PTYPE
DRIVER, PTYPE

Three-Factor Models

RTYPE, SYSTEM, PLANT	
RYPTE, OPMODE, PLANT	
RTYPE, PTYPE, PLANT	
RTYPE, DRIVER, PLANT	
RTYPE, SYSTEM, OPMODE	
RTYPE, SYSTEM, PTYPE	
RTYPE, SYSTEM, DRIVER	
RTYPE, SYSTEM, PTYPE	
SYSTEM, PTYPE, OPMODE	
SYSTEM, DRIVER, OPMODE	
PTYPE, DRIVER, OPMODE	
PTYPE, RTYPE, OPMODE	
DRIVER, RTYPE, OPMODE	
DRIVER, SYSTEM, PTYPE	

P-Value	s	
0.2364	x	10-1
0.2973	x	10-1
0.3389	x	10-2
0.6060	x	10-1
0.1532	x	10-1
0.2285	x	10-2
0.6255	x	10-1
0.4114	X	100

 0.1496×10^{0} 0.2727×10^{-2} 18

4

40

The

TABLE B-I (cont)

Four-Factor Models	
RTYPE, PLANT, SYSTEM,	OPMODE
RTYPE, PLANT, SYSTEM,	PTYPE
RTYPE, PLANT, SYSTEM,	DRIVER
RTYPE, PLANT, OPMODE,	PTYPE
RTYPE, PLANT, OPMODE,	DRIVER
RTYPE, PLANT, PTYPE,	DRIVER
SYSTEM, RTYPE, DRIVER	, OPMODE
SYSTEM, RTYPE, DRIVER	R, PTYPE
SYSTEM, RTYPE, OPMODE	, PTYPE
DRIVER, RTYPE, OPMODE	, PTYPE
DRIVER, SYSTEM, OPMOL	DE, PTYPE

4

0.3912			
0.4265	x	10-2	
0.5271	x	10-2	
0.2191	x	10-1	
0.9620	x	10-1	
0.2473	x	10-2	

P-Values

and the second s	and the second second	100 - D D
F 8 37 62	Factor	Modele
5 A V C	TRUCUL	110110 10

-

P-Values

TYPE, PLANT, SYSTEM, OPMODE, PTYPE	
TYPE, PLANT, SYSTEM, OPMODE, DRIVER	
TYPE, PLANT, SYSTEM, DRIVER, PTYPE	
TYPE, PLANT, OPMODE, PTYPE, DRIVER	
TYPE, SYSTEM, PTYPE, DRIVER, OPMODE 0.4270 x	10-2

Six-Factor Model

P-Value

RTYPE, PLANT, OP/ODE DRIVER, PTYPE, SYSTEM

TABLE B-II

DEGRADED DEMAND-RELATED MSS FRAC MODEL

Average Failure Rate Estimate--1.51 x $10^{-2}(8.091 \times 10^{-3})$

Fixed Factors

Level of Influence	Factor	Level	Description	Rj	Failure Rate Adjustment
1	SYSTEM	1	Nuclear	27.78	5.00 (2.188)
		2	Engineered Safety		3.00 (2.037)
		3	Containment		0.39 (0.441)
		4	Electrical		0.34 (0.250)
		5	Power Conversion		0.18 (0.282)
		6	Process Auxiliary		2.10 (0.923)
		7	Plant Auxiliary		1.31 (0.774)
2	DRIVER	1	Motor	10.52	0.99 (0.542)
		2	Diesel		3.26 (1.389)
		3	Turbine		0.31 (0.200)

Random Factor

Factor

ERROR

Variance Component

3.186

TABLE B-III

BEST AND WORST CASE DEGRADED DEMAND-RELATED FRAC PUMP FAILURE RATE ESTIMATES

Case	SYSTEM	DRIVER	Estimate
Best	Power Conversion	Turbine	$8.64 \times 10^{-5}/d$
Worst	Nuclear	Diesel	$2.49 \times 10^{-1}/d$

Note: $2.49 \times 10^{-1}/8.64 \times 10^{-5} = 2882 \approx 3.5$ orders of magnitude between the best and worst case estimates.

One-Factor Models RTYPE SYSTEM OPMODE PTYPE DRIVER

P-Value 0.1344 x 10⁻⁶ 0.1393 x 10⁻² 0.9042 0.1504 0.9503

Two-Factor Models

P-Value

RTYPE, PLANT RTYPE, SYSTEM RTYPE, OPMODE RTYPE, PTYPE RTYPE, DRIVER SYSTEM, OPMODE SYSTEM, PTYPE SYSTEM, DRIVER OPMODE, DRIVER OPMODE, PTYPE DRIVER, PTYPE

Three-Factor Models

RTYPE, SYSTEM, PLANT RTYPE, OPMODE, PLANT RTYPE, PTYPE, PLANT RTYPE, DRIVER, PLANT RTYPE, SYSTEM, OPMODE RTYPE, SYSTEM, PTYPE RTYPE, SYSTEM, DRIVER RTYPE, SYSTEM, PTYPE SYSTEM, PTYPE, OPMODE SYSTEM, DRIVER, OPMODE PTYPE, RTYPE, OPMODE DRIVER, RTIPE, OPMODE DRIVER, SYSTEM, PTYPE $\begin{array}{c} 0.5548 \times 10^{-8} \\ 0.9165 \times 10^{-6} \\ 0.7489 \times 10^{-6} \\ 0.3316 \times 10^{-5} \\ 0.2208 \times 10^{-2} \\ 0.1642 \times 10^{-2} \\ 0.6158 \times 10^{-2} \\ 0.9959 \\ 0.2933 \\ 0.5301 \end{array}$

P-Value

-----0.1704 x 10⁻⁷ 0.1707 x 10⁻⁷ 0.4090×10^{-7} 0.9400 x 10⁻⁵ 0.3291×10^{-2} 0.8709 × 10⁻² 0.6328 0.3374 x 10⁻⁵ 0.1104 × 10⁻⁴ 0.6690×10^{-2}

DEGRADED DEMAND-RELATED FRAC FAILURE RATE MODEL ANALYSIS

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TABLE B-IV (cont)

Four-Factor Models

RTYPE,	PLANT,	SYSTEM,	OPMODE
RTYPE,	Planit,	SYSTEM,	PTYPE
RTYPE,	PLANT,	SYSTEM,	DRIVER
RTYPE,	PLANT,	OPMODE,	PTYFE
RTYPE,	PLANT,	OPMODE,	DRIVER
RTYPE,	PLANT,	PTYPE,	DRIVER
SYSTEM,	RTYPE	DRIVER	, OPMODE
SYSTEM,	RTYPE	, DRIVER	, PTYPE
SYSTEM,	RTYPE	, OPMODE	, PTYPE
DRIVER,	RTYPE	, OPMODE	, PTYPE
DRIVER,	SYSTE	M, OPMOD	E, PTYPE

Five-Factor Models

RTYPE,	PLANT,	SYSTEM,	OPMODE,	PTYPE	
RTYPE,	PLANT,	SYSTEM,	OPMODE,	DRIVER	
RTYPE,	PLANT,	SYSTEM,	DRIVER,	PTYPE	
RTYPE,	PLANT,	OPMODE,	PTYPE, I	DRIVER	
RTYPE,	SYSTEM	, PTYPE,	DRIVER,	OPMODE	

-					
-					
-					
-					
-					
-					
0	.1116	x	10-6	1	
0	.1121	x	10-6		
0	.4927	x	10-7		$\langle \rangle$
0	.2860	x	10-4	1	Y
0	.1186	x	10-1		

P-Value

-Val	ue	 	

0.2919	*	10-1	6

Six-Factor Model

RTYPE, PLANT, SYSTEM OPMODE, PTYPE, DRIVER

P-Value

TABLE B-V

INCIPIENT DEMAND-RELATED MSS FRAC MODEL

Average Failure Rate Estimate--4.13 x $10^{-2}(7.541 \times 10^{-3})$

Fixed Factors

Level of Influence	Factor	Level	Description	Rj	Failure Rate Adjustment
1	SYSTEM	1 2 3 4 5 6 7	Nuclear Engineered Safety Containment Electrical Power Conversion Process Auxiliary Plant Auxiliary	12.45	2.04 (0.463) 1.46 (0.378) 0.57 (0.279) 0.29 (0.172) 0.30 (0.228) 1.87 (0.413) 3.61 (0.980)
2	RTYPE	1 2	PWR BRW	2.90	1.71 (0.156) 0.59 (0.054)

Random Factor

Factor

ERROR

Variance Component

3.273

TABLE B-VI

BEST AND WORST CASE DEGRADED DEMAND-RELATED FRAC PUMP FAILURE RATE ESTIMATES

Case	SYSTEM	RTYPE	Estimate
Best	Electrical	BWR	$7.00 \times 10^{-3}/d$
Worst	Plant Auxiliary	PWR	$2.55 \times 10^{-1}/d$

Note: $2.55 \times 10^{-1}/7.00 \times 10^{-3} = 36.43 \approx 1.6$ orders of magnitude between the best and worst case estimates.

APPENDIX C

DEGRADED AND INCIPIENT TIME-DEPENDENT PUMP FAILURE RATE ANALYSES

TABLE C-I

DEGRADED TIME-DEPENDENT FRAC FAILURE KATE MODEL ANALYSIS

One-Factor	Models
RTYPE	
SYSTEM	
OPMODE	
PTYPE	
DRIVER	

0.1805 0.0993 0.5078

Two-Factor Models

P-Values

0.1696

0.2501

0.4016

0.3764

0.0153

C.1792

0.1691

0.5640

0.8220

0.9365

RTYPE, PLANT RTYPE, SYSTEM RTYPE, OPMODE RTYPE, PTYPE RTYPE, DRIVER SYSTEM, OPMODE SYSTEM, PTYPE SYSTEM, DRIVER OPMODE, DRIVER OPMODE, PTYPE DRIVER, PTYPE

Three-Factor Models

RTYPE, PLANT, SYSTEM RTYPE, PLANT, OPMODE RTYPE, PLANT, PTYPE RTYPE, PLANT, DRIVER RTYPE, SYSTEM, OPMODE RTYPE, SYSTEM, PTYPE RTYPE, SYSTEM, DRIVER RTYPE, PTYPE, SYSTEM

PTYPE, SYSTEM, OPMODE DRIVER, OPMODE, SYSTEM OPMODE, PTYPE, DRIVER RTYPE, PTYPE, OPMODE RTYPE, DRIVER, OPMODE

SYSTEM, DRIVER, PTYPE

P-Values	
0.0165	
0.2115	
0.3145	
0.2545	4
0.0021	
0.0397	
0.0447	
0.5858	
0.0253	
0.0285	
0.7671	
0.4387	
0.2847	

0.2693

46

8

TABLE C-I (cont)

Four-Factor Models	P-Values
RTYPE, PLANT, SYSTEM, OPMODE	0.0035
RTYPE, PLANT, SYSTEM, PTYPE	0.0249
RTYPE, PLANT, SYSTEM, DRIVER	0.0121
RTYPE, PLANT, OPMODE, PTYPE	0.3386
RTYPE, PLANT, OPMODE, DRIVER	0.1724
RTYPE, PLANT, PTYPE, DRIVER	0.3957
SYSTEM, RTYPE, DRIVER, OPMODE	0.0031
RTYPE, PTYPE, DRIVER, SYSTEM	0.0561
PTYPE, SYSTEM, OPMODE, RTYPE	0.0049
DRIVER, OPMODE, RTYPE, PTYPE	0.4516
OPMODE, PTYPE, DRIVER, SYSTEM	0.0424

Five-Factor Models

RTYPE,	PLANT,	SYSTEM,	OPMODE,	PTYPE
RTYPE,	PLANT,	SYSTEM,	OPMODE,	DRIVER
RTYPE,	PLANT,	SYSTEM,	DRIVER,	PTYPE
RTYPE,	PLANT,	OPMODE,	PTYPE, I	DRIVER
RTYPE,	SYSTEM.	PTYPE,	DRIVER,	OPMODE

Si--Factor Model

RTYPE, PLANT, OPMODE DRIVER, PTYPE, SYSTEM

P-Values

0.6799	x	10-2	
0.2790	x	10-2	$\langle $
0.1892	x	10-1	4
0.2483	x	100	
0.6725	x	10-2	

P-Value

 0.5099×10^{-2}

TABLE C-II

DEGRADED TIME-DEPENDENT MSS FRAC MODEL

Average Failure Rate Estimate--4.70 x $10^{-5}(3.90 \times 10^{-5})$

Fixed Factors

Level of Influence	Factor	Level	Description	Rj	Failure Rate Adjustment
1	SYSTEM	1	Nuclear	33.40	2.79 (2.361)
		2	Engineered Safety		0.15 (0.373)
		3	Power Conversion		5.01 (4.644)
		4	Process Conversion		0.47 (0.411)
2	OPMODE	1	Running	4.93	0.45 (0.129)
		2	Alternating		2.22 (0.634)
3	RTYPE	1	PWR	2.24	1.50 (0.244)
		2	BWR		0.67 (0.109)

Random Factor

Factor	Variance Component
ERROR	3.521

TABLE C-- III

BEST AND WORST CASE DEGRADED TIME-DEPENDENT FRAC PUMP FAILURE RATE ESTIMATES

Case	SYSTEM	OPMODE	RTYPE	Estimate
Best	Engineered Safety	Running	BWR	$2.13 \times 10^{-6}/h$
Worst	Power Conversion	Alternating	PWR	$7.84 \times 10^{-6}/h$

Note: $7.84 \times 10^{-4}/2.13 \times 10^{-6} = 368.08 \approx 2.6$ orders of magnitude between the best and worst case estimates.

ne-Factor Models	
TYPE	
SYSTEM	
PMODE	
TYPE	
DRIVER	

INCIPIENT TIME-DEPENDENT FRAC FAILURE RATE MODEL ANALYSIS

Two-Factor Models

RTYPE, PLANT RTYPE, SYSTEM RTYPE, OPMODE RTYPE, PTYPE RTYPE, DRIVER SYSTEM, OPMODE SYSTEM, PTYPE SYSTEM, DRIVER OPMODE, DRIVER OPMODE, PTYPE DRIVER, PTYPE

P-Value	s		
0.1302	x	10-4	
0.1335	x	10 ⁻⁵	
0.1004	x	10 ⁻⁵	
0.4100	x	10 ⁻⁷	4
0.5951	x	100	
0.2613	x	100	
0.6435	x	10-1	
0.4538	x	10-1	
0.1933	x	100	
0.4442	×	10-2	

P

P-Values

0.2848 x 10⁻⁶ 0.4408 x 10⁰ 0.3981×10^{0} 0.8205×10^{-1} 0.1245 x 10⁻¹

Three-Factor Models
RTYPE, PLANT, SYSTEM
RYPTE, PLANT, OPMODE
RTYPE, PLANT, PTYPE
RTYPE, PLANT, DRIVER
RTYPE, SYSTEM, OPMODE
RTYPE, SYSTEM, PTYPE
RTYPE, SYSTEM, DRIVER
RTYPE, PTYPE, DRIVER
OPMODE, PTYPE, SYSTEM
OPMODE, DRIVER, SYSTEM
OPMODE, DRIVER, PTYPE
OPMODE, RTYPE, PTYPE
OPMODE, RTYPE, DRIVER
SYSTEM, PTYPE, DRIVER

i,

P-Value	s		<u>.</u>
0.3907	x	10-4	
0.2057	x	10-4	
0.1623	x	10-5	4
0.5614	x	10-7	$\langle 1 \rangle$
0.2587	x	100	4
0.1084	x	100	
0.1125	x	10 ⁻¹	
0.3623	x	10 ⁻⁵	
0.2034	x	10-6	
0.3545	x	10-1	

TABLE C-IV (cont)

Four-Fa	actor Me	odels	
RTYPE,	PLANT,	SYSTEM,	OPMODE
RTYPE,	PLANT,	SYSTEM,	PTYPE
RTYPE,	PLANT,	SYSTEM,	DRIVER
RTYPE,	PLANT,	OPMODE,	PTYPE
RTYPE,	PLANT,	OPMODE,	DRIVER
RTYPE,	PLANT,	PTYPE,	DRIVER
RTYPE,	OPMODE	, SYSTEM	, DRIVER
RTYPE,	PTYPE,	DRIVER,	SYSTEM
RTYPE,	PTYPE,	OPMODE,	SYSTEM
RTYPE,	PTYPE,	OPMODE,	DRIVER
SYSTEM.	, PTYPE	, OPMODE	, DRIVER

$\begin{array}{c} \hline & & \\ 0.4697 \times 10^{-5} \\ 0.2031 \times 10^{-5} \\ 0.4293 \times 10^{-4} \\ 0.2005 \times 10^{-6} \\ 0.3409 \times 10^{-1} \end{array}$

P-Values

Five-Factor Models

RTYPE, PLANT, SYSTEM, OPMODE, PTYPE RTYPE, PLANT, SYSTEM, OPMODE, DRIVER RTYPE, PLANT, SYSTEM, PTYPE, DRIVER RTYPE, PLANT, OPMODE, PTYPE, DRIVER RTYPE, SYSTEM, OPMODE, PTYPE, DRIVER -

P-Values

 0.3649×10^{-5}

P-Values

Six-Factor Model

RTYPE, PLANT, SYSTEM, OPMODE PTYPE, DRIVER

TABLE C-V

INCIPIENT TIME-DEPENDENT MSS FRAC MODEL

Average Failure Rate Estimate $-3.65 \times 10^{-4} (5.02 \times 10^{-5})$

			Fixed Factors		
evel of	Factor	Level	Description	Rj	Failure Rate Adjustment
1	RTYPE	1	PWR	3.31	1.82 (0.181)
		2	BWR		0.55 (0.055)
2	DRIVER	1	Motor	2.16	0.68 (0.093)
		2	Turbine		1.47 (0.201)
			Random Factor		
	Factor			Variance Component	
	ERROR				5.596

TABLE C-VI

BEST AND WORST CASE INCIPIENT TIME-DEPENDENT FRAC PUMP FAILURE RATE ESTIMATES

Case	RTYPE	DRIVER	Estimate
Best	BWR	Motor	$1.37 \times 10^{-4}/h$
Worst	PWR	Turbine	$9.77 \times 10^{-4}/h$

Note: $9.77 \times 10^{-4}/1.37 \times 10^{-4} = 7.13 \approx 0.9$ orders of magnitude between the best and worst case estimates.

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PERFORMING ORGANIZATION MAME AND MAILING ADDRESS Haclude Zop Codes Los Alamos National Laboratory Los Alamos, New Mexico 87545	10 FIN NUMBER A7725		
Division of Risk Analysis Office of Nuclear Regulatory Research	12. TYPE OF REPOR	Informal	
US Nuclear Regulatory Commission Washington, DC 20555	125 PERIOD COVERI	ED (Inclusive dates)	
13 SUPPLEMENTARY NOTES			
 ABSTRACT 1200 work or MU In-Plant Reliability Data System (IPRDS) pump in four nuclear power plants are statistically analy Code (FRAC). A major purpose of the analysis is to system, and operating factors adequately explain the Catastrophic, degraded, and incipient failures sever: demand-related and time-dependent failures. For catastrophic demand-related pump failures, following factors listed in their order of inportant operating mode, reactor type, pump type, and uniden Quantitative failure rate adjustments are provided In the case of catastrophic time-dependent pum is explained by three factors: reactor type, pump influences. Finally, point and confidence interval failure selected pump by considering the influential factor an improvement over the estimates computed exclusiv 	failure data on over yzed using the Failu determine which env e variability in the ity categories are of the variability is ce: system applicat tified plant-specifi for the effects of t p failures, the fail driver, and unident nate estimates are s. Both types of es ely from the data of	60 selected pumps are Rate Analysis ironmental, failure data. considered for both explained by the tion, pump driver, to influences. these factors. ture rate variability ified plant-specific provided for each stimates represent n each pump.	
16 AVAILABILITY STATEMENT 17 Unlimited 19	SECURITY CLASSIFICATION (This report) Unclassified SECURITY CLASSIFICATION	18 NUMBER OF PAGES	
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OUS. GOVERNMENT PRINTING OFFICE: 1984-0-776-026/4027

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