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R5FORCE: A PROGRAM TO COMPUTE FLUID INDUCED FORCES USING HYDRODYNAMIC OUTPUT FROM THE RELAPS CODE

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INTERIM REPORT





ABSTRACT

This report describes the development of a computer program which operates on hydrodynamic output from the RELAP5/MOD1 program and computes piping hydrodynamic force/time histories for input into various structural analysis codes. The report describes the force calculation theory, showing the development of a general force equation and the solution of this equation within the RELAP5 output structure. To illustrate the calculational method and provide results for discussion, a sample problem is presented. A detailed user manual for the computer program is included as an appendix.

The work was performed in support of the NRC Safety/Relief Valve Program for which EG&G Idaho acted as the System Integrator. SUMMARY

This report describes the development of a computer program that uses hydrodynamic output from the RELAP5/MOD1 program and computes piping hydraulic force/time histories for input into various structural analysis codes. This program is considered an improvement over existing force calculation techniques available at EG&G Idaho because it solves the force equation using the pressure and wall shear force terms instead of the pressure and fluid acceleration terms, eliminating potential instabilities associated with computing the time derivative in the fluid acceleration term; and uses output from the RELAP5/MOD1 program, an advanced one-dimensional computer program which is fast, accurate and easy to use.

A general equation was constructed to describe the force exerted on a container. This general equation is applicable to a wide variety of pipe force situations and serves as the fundamental relationship for the calculation program. Forces are computed for each RELAP5 hydrodynamic control volume, then summed over designated control volumes to obtain the total force.

The computer program R5FORCE is designed to operate on input, output and calculational phases. During the input phase, system geometry data and user input data are read, stored in memory, and then used to set up control arrays. The calculation phase involves a progression through the RELAP5 output data where all required forces are computed and written to an output file. Upon completion of the requested force calculations, the program provides a summary identifying the maximum positive and negative forces encountered for each volume force, subforce and combined force requested, including the time of the maximum force.

A sample problem was considered to illustrate the calculational technique and provide results for discussion. Two sample problems were used to create results for comparison with existing force calculation techniques available at EG&G Idaho, Inc. The same system was used for both sample problems and consisted of a supply vessel connected by a valve to an



accumulator which was then connected to a relief valve through a short length of piping; a section of relief valve discharge piping was also included. The first transient consisted of a steam filled relief valve inlet line in which the supply vessel pressure was increased until the relief valve opened. The valve separating the supply vessel and the accumulator was then closed, allowing the accumulator to blowdown until the relief valve closed. The second transient was identical to the first except the loop seal in the relief valve inlet piping was filled with subcooled liquid. Force calculations were performed for each transient and results are presented later in this report.

A detailed user manual for R5FORCE is included as an appendix to this report.

CONTENTS

	ABSTI	RACT	11			
	SUMM	ARY	iii			
	1.	INTRODUCTION	1			
	2.	FORCE CALCULATION THEORY	3			
		2.1 General Equation	3			
		2.2 Continued Junction	6			
		2.3 Bounded Junction	8			
		2.4 Open Junction	9			
		2.5 Special Junction	9			
	3.	COUPLING TO RELAPS	11			
	4.	THE COMPUTER PROGRAM	13			
	5.	SAMPLE PROBLEM				
	6.	COMPARISON WITH EXISTING TECHNIQUES	24			
	7.	CONCLUSIONS				
	8.	. REFERENCES				
APPENDIX ADEVELOPMENT OF THE GENERAL FORCE EQUATION						
	APPE	NDIX BDEVELOPMENT OF THE JUNCTION PRESSURE AND JUNCTION AREA TERMS	B-i			
	APPE	NDIX CDEVELOPMENT OF THE SHEAR FORCE COMPONENT AND MODIFICATION OF THE RELAP5 ROUGHNESS TERM	C-i			
	APPE	NDIX DRELAP5 CODE UPDATES AND OUTPUT TAPE FORMAT	D-i			
	APPE	NDIX ER5FORCE PROGRAM LISTING (MICROFILM)	E-i			
	APPE	NDIX FPROGRAM USERS GUIDE	F-1			
	APPE	NDIX GSAMPLE PROBLEM INPUT PROCESSING DESCRIPTION	G-i			
	APPE	NDIX HSAMPLE PROBLEM OUTPUT SUMMARY	H-i			

FIGURES

1.	Generalized fluid container	4
2.	Typical piping/control volume system	7
3.	R5FORCE flow diagram	14
4.	Piping system for sample problem	17
5.	Sample piping system showing selected forces	19
6.	Subforces SF101 and SF103 for the sample problem	20
7.	Combined force CF201 for the sample prob'en	21
8.	Subforces SF102, SF104 and SF106 for the sample problem	22
9.	Combined force CF202 for the sample problem	23
10.	Comparison of the old, modified and new approaches for subforce SF105 for the sample problem	26
11.	Comparison of the old, modified and new approaches for subforce SF108 for the sample problem	27
12.	Comparison of the old, modified and new approaches for combined force CF203 for the sample problem	28
13.	Comparison of the old, modified and new approaches for subforce SF105 for the second sample problem	29
14.	Comparison of the old, modified and new approaches for subforce SF108 for the second sample problem	30
15.	Comparison of the old, modified and new approaches for combined force CF203 for the second sample problem	31
16.	Modified approach for combines force CF203 for the second sample problem from 0.2 to 0.5 seconds	32
17.	New approach for combined force CF 203 for the second sample problem from 0.2 to 0.5 seconds	33

R5FORCE: A PROGRAM TO COMPUTE FLUID INDUCED FORCES USING HYDRODYNAMIC OUTPUT FROM THE RELAPS CODE

1. INTRODUCTION

There are currently available a number of computer programs (such as RELAP5¹ and TRAC²) that have the capability of simulating the transient and steady-state flow behavior in piping systems under both single and two-phase flow conditions. In each of these programs, the primary effort was directed towards predicting the flow behavior in the piping system but did not included the calculation of fluid induced forces. For the design and analysis of piping systems (such as relief valve discharge piping, or systems undergoing pipe rupture, or abnormal valve or pump operation), fluid forces on the piping are an important portion of the overall structural analysis and must be computed.

This report describes the development of a computer program that operates on hydrodynamic output from the RELAP5/MOD1 program and computes piping hydraulic force/time histories for input into various structural analysis codes, such as NUPIPE, ³ SAP⁴ OR ADINA⁵. This program is considered an improvement over existing force calculation techniques available at EG&G Idaho (References 6 and 7) because it solves the force equation using the pressure and wall shear force terms instead of the pressure and fluid acceleration terms, eliminating potential instabilities associated with computing the time derivative in the fluid acceleration term; and uses output from the RELAP5/MOD1 program, an advanced one-dimensional computer program that is fast, accurate and easy to use.

Section 2 of this report is a description of the force calculation theory showing the development of a general force equation and how it applies to various system geometries. Section 3 details how these force equations are then solved within the RELAP5 output structure. The resulting computer program R5FORCE is described in Section 4. To illustrate the calculational method and provide results for discussion, a sample problem is considered in Section 5. In Section 6, this sample problem and a slightly modified form of this problem are used in a comparison study with previously existing calculational techniques available at EG&G Idaho. Section 7 includes several conclusions from this work. A detailed user manual for the R5FORCE program is included as an appendix to this report.

This work was conducted for the Nuclear Regulatory Commission's Safety/Relief Valve Program and fulfills a portion of the task described in References 7 and 8. This report will assist in auditing utility safety/relief valve system analyses as requested by the NRC.

2. FORCE CALCULATION THEORY

2.1 General Equation

It is possible to derive a general equation for the net force exerted on a container based upon the following assumptions:

- 1. Neglect external fluid velocity and shear force effects
- 2. One-dimensional uniform cross sectional area control volume
- Normal stress approximated by the quasi steady change in momentum (the local dynamic pressure plus the fluid momentum)
- Uniform fluid velocity, density, and pressure over the local cross sectional area and uniform shear over the local control volume surface area.

Based on the cross sectional view of the arbitrary shaped container and the notation specified in Figure 1, this equation can be expressed as

 $F = -(P_{II} + \rho_I u_I^2) A_{II} + (P_{I2} + \rho_I u_I^2) A_{I2} + P_{EI} A_{EI} - P_{E2} A_{E2} + \tau A_s$ (1)

3

where

p

- A = volume surface area
 P = fluid pressure
 u = fluid velocity
 - = fluid density

τ = shear force per unit area



and the subscripts (1) and (E) refer to interior or external conditions, the subscripts (1) and (2) refer to the volume inlet or outlet and the subscript (s) refers to the interior surface area parallel to the flow. The first four terms in this equation represent the forces resulting from the pressure and momentum at Control Surfaces CS1 and CS2. The fifth term represents the force resulting from fluid shear on Control Surface CS3. Starting from basic principles, a detailed development of Equation (1) is included in Appendix A. This equation applies to a wide variety of pipe force situations and serves as the fundamental relationship for the calculation program described herein.

A dynamic structural analysis of a piping system requires that forces be applied, in terms of time histories, at various points or node locations in the piping model. These nodes are generally located near components that result in either a change in flow direction or flow area (Such as elbows or bends, reducers, valves or an open pipe end). Since the application of Equation (1) makes it possible to compute a net force for each volume in the hydrodynamic analysis, the total force at any particular node location can be considered to be the sum of the individual forces of each hydrodynamic volume within the control volume defining the nodal force.

Equation (1) is made up of five terms. Two of these terms represent forces associated with the volume inlet junction, two with the volume outlet junction and one with the volume itself. The application of Equation (1) will differ depending on the type of volume end geometry. In particular, a volume can be connected to an adjoining volume in one of four ways:

 Continued--Adjacent volumes are at the same angle, such as Volumes CV2 and CV3 in Figure 2

 Bounded--Adjacent volumes are at different angles, such as Volumes CV3 and CV4 in Figure 2



- Open--A volume represents the end of a pipe, although continued to an adjacent volume in the RELAP5 model, such as Volume CV4 in Figure 2
- Special--Mechanistic junction models, such as the relief valve between Volumes CV1 and CV2 in Figure 2.

These geometries can also contain area changes between adjacent volumes and a constant or variable throat ratio, simulating an orifice or a valve. Each of these geometries will be discussed in greater detail below.

2.2 Continued Junction

From the previous discussion, the junction connecting Volumes CV2 and CV3 in Figure 2 can be considered to be continued since there is no change in direction between the adjacent volumes. Applying the applicable portions of Equation (1) to the inlet and outlet junctions of a general hydrodynamic control volume results in:

$$F_{1} = -(P_{11} + \rho_{1} u_{1}^{2}) A_{11} + P_{E1} A_{E1}$$

$$F_2 = (P_{12} + P_1 u_1^2) A_{12} - P_{E2} A_{E2}$$

where

р	=	fluid	pressure	
ρ	=	fluid	density	
ū	=	fluid	velocity	
A	=	area		

-



Figure 2. Typical piping/control volume system.

and the subscripts (I) and (E) refer to internal and external conditions, and the subscripts (1) and (2) refer to the inlet and outlet junctions of a control volume, respectively. Thus, there are four internal parameters (P, ρ , u, A) and two external parameters (P, A) that must be determined for the inlet and outlet junction of each control volume.

The external pressure at the inlet and outlet junction are available from the input data to R5FOR(.. The internal change in momentum and area at the inlet and outlet junction are not available directly in RELAP5, however, they can be computed as discussed in Appendix B.

2.3 Bounded Junction

The junction connecting Volumes CV3 and CV4 in Figure 2 can be considered to be bounded since there is a change in direction between adjacent volumes. Applying the applicable portions of Equation (1) to the inlet and outlet junctions of a general hydrodynamic control volume results in:

$$F_{1} = -(P_{11} + P_{1} u_{1}^{2}) A_{11} + P_{E1} A_{E1}$$

 $F_2 = (P_{12} + P_1 u_1^2) A_{12} - P_{E2} A_{E2}$

Note: When the $(P + \rho u_I^2)(A)$ term was evaluated for a continued type of junction, the $(P + \rho u_I^2)$ term corresponded to the pressure and momentum approximated from volume conditions impinging on a flow area restriction. For a bounded type of junction, this force will still exist in addition to the force resulting from the pressure and momentum at the junction acting on the pipe during the bend. Expanding the above expressions to account for these force developing areas results in:



$$F_{1} = -(P_{I1} + P_{I} u_{I}^{2}) A_{I1} - (P_{I1} + P_{IJ1} u_{IJ1}^{2}) A_{IJ1} + P_{E1} A_{E1}$$

$$F_2 = (P_{I2} + \rho_I u_I^2) A_{I2} + (P_{I2} + \rho_{IJ2} u_{IJ2}^2) A_{IJ2} - P_{E2} A_{E2}$$

where the subscript (J) refers to junction conditions.

Note: Since the force on each hydrodynamic control volume is computed, then summed over one or more control volumes with the same elevational angle, the results will be independent of the geometric relationship of the volumes on the other side of a bend. Thus, the results are not dependent on any particular bend angle.

2.4 Open Junction

The outlet junction of Volume CV4 in Figure 2 can be considered to be open, representative of the end of a pipe. Since an open pipe is at the outlet of a piping system, only the outlet junction of a volume will be considered to be open. Applying the applicable portions of Equation (1) to the outlet junction of a general hydrodynamic control volume results in:

$$F_2 = (P_{12} + \rho_1 u_1^2) A_{12} - P_{E2} A_{E2}$$

2.5 Special Junction

Because of the physical differences between an actual relief valve and the RELAP5 model of a relief valve, the junction connecting Volumes CV1 and CV2 in Figure 2 must be treated with a special mechanistic model. Two special mechanistic models currently exist in the code, one of which is a relief valve model with the orifice on the inlet and the other is a relief valve with the orifice on the outlet. Both of these mechanistic models assume the control volumes connected to the relief valve inlet and outlet are at an angle to each other. Applying the applicable portions of Equation (1) to the valve inlet (outlet junction of the preceding control volume) and outlet (inlet junction of the following control volume) where the orifice is on the valve outlet results in:

$$F_{1} = -(P_{I1} + P_{I} u_{I}^{2}) A_{I1} - (P_{IJ1} + P_{IJ1} u_{IJ1}^{2}) A_{IJ1} + P_{E1} A_{E1}$$

 $F_2 = (P_{12} + P_1 u_1^2) A_{12} - P_{E2} A_{E2}$

where the value outlet force (F_1) is defined as though it were a bounded junction and the value inlet force (F_2) is defined as though it were a continued junction, except that area A_{12} is the full area of the pipe. For the case of the relief value orifice being on the value inlet, the above equations would be reversed.



3. COUPLING TO RELAP5

The numerical solution of the two-phase flow equations in RELAP5 is accomplished through the use of a spatial mesh of hydrodynamic control volumes connected by junctions. Fluid properties are defined at the center of each control volume (such as pressure, density and velocity) and at each junction (such as density and velocity). The application of Equation (1) makes it possible to compute a net force for each hydrodynamic control volume in the RELAP5 analysis. In general, each force control volume includes one or more control volumes. Moreover, the force acting on each control volume can be computed, then summed over an entire force control volume.

Examining Equation (1) yields several flow quantities that must be obtained from RELAP5 in order to evaluate the forces acting on a control volume.

These include the following:

- 1. Control volume pressure
- 2. Control volume momentum
- 3. Junction momentum
- 4. Indication of choking at a junction
- 5. Control volume shear force.

The control volume pressure is readily available as are the momentum terms and the indication of junction choking. However, both the control volume momentum and junction momentum must be modified for a two-phase flow situation as:

 $\rho u^2 = \alpha_g \rho_g u_g^2 + (1-\alpha_g) \rho_f u_f^2$

where α is the void fraction and the subscripts (g) and (f) refer to the gas and fluid phases, respectively.

The control volume shear force term is not available directly in RELAP5, however, it can be computed as discussed in Appendix C. To correctly compute the fluid shear however, system components resulting in a frictional loss, such as elbows, must be modeled by modifing the volume roughness rather than by adding an energy loss coefficient at a junction. Modification of the volume roughness is also contained in Appendix C.

Using the internally computed properties, the following quantities are written to the RELAP5 output tape at every successful time step.

1. For each volume:

- a. Control volume pressure
- b. Total wall shear
- c. Control volume momentum
- 2. For each junction:
 - a. Junction throat ratio
 - b. Junction momentum
 - c. Indication of junction choking

This information can then be used to compute the force on any RELAP5 control volume then summed over designated control volumes to obtain the total force.

4. THE COMPUTER PROGRAM

The computer program that solves the force equations and creates a force/time history is entitled R5FORCE. The program uses output data from RELAP5 in the format described in Appendix C; the code updates used to create this data file are also included in this appendix.

Figure 3 shows that R5FORCE operates in an input, calculational and output phase. During the input phase, system geometry data (available on the RELAP5 output tape) and user input data are read and stored in memory. This data is then used to set up integer control arrays that contain such information as the force reference numbers, direction indicator flags, and applicable RELAP5 junction and control volume numbers. Once the control arrays are established the calculation phase involves a progression through the RELAP5 output data, where all required forces are computed (at each RELAP5 computational time step) and then written to an output file; forces can also be printed at selected time steps. Upon completion of the requested force calculations, the program provides a summary identifying the maximum positive and negative forces encountered for each volume force, subforce, and combined force requested, including the time of the maximum force. In addition, each computed force can be output in a format suitable for plotting. Pressures at each RELAP5 control volume can also be written to an output file for use as input to structural analysis codes.

In order to be consistent with the basic equations solved in R5FORCE, the following conventions must be followed.

- The RELAP5 model must be developed in the direction of positive flow.
- The force direction must be colinear with the pipe axis, in any direction.



- 3. System components resulting in a frictional loss, such as elbows, must be modeled by modifing the volume roughness term, not by the addition of an energy loss coefficient. Note: The roughness cannot be larger than half the volume diameter.
- Branch components in RELAP5 cannot be included in the definition of a subforce or a combined force.

R5FORCE has been written using Control Data Corporation (CDC) FORTRAN Version 5. The intrinsic functions SHIFT, MASK, LOCF, CMMALF and ENCODE, which are CDC extensions to FORTRAN 77, are utilized and therefore make the program CDC dependent. A listing of R5FORCE is included in Appendix E.



5. SAMPLE PROBLEM

A sample problem is now considered in order to illustrate the application of the methods considered previously, and also to provide results for discussion. Detailed user input instructions for this sample problem are discussed in Appendix F of this report.

The sample problem consisted of a simple relief system as shown in Figure 4. The system involved a pressurized accumulator connected to a relief valve through a short length of piping which served as a loop seal. The relief valve discharge piping terminated as an open pipe segment.

A RELAP5/MOD1 hydrodynamic model of this system was used to generate an input file for force calculations. This model consisted of fluid control volumes connected by junctions and extended through the entire piping system. Each control volume and junction was described in terms of fluid state, geometry, and flow characteristics, with locations selected to ensure adequate representation of the fluid transient.

Upstream from the relief valve, the accumulator and piping initially contained saturated steam at a pressure of 16.55 MPa that was increased linearly to 18.27 MPa in 0.5 s. The discharge piping was assumed to be initially filled with saturated steam at atmospheric pressure; the downstream boundary was maintained at this pressure. The fluid transient considered involved a 40 ms relief valve opening beginning when the relief valve inlet pressure reached 17.24 MPa, which occurred at 0.21 s. Following the valve opening, steady flow in the piping was achieved at approximately 0.5 s, once the supply pressure stopped increasing. The valve separating the supply vessel and the accumulator remained open until 1.0 s, at which time it was closed, allowing the accumulator to blowdown until the relief valve closed at 16.38 MPa at 1.44 s. The problem was terminated at 2.0 s.



A description of the various subforce and combined forces selected for discussion is shown in Figure 5. Figure 6 is a force/time history of subforces SF101 and SF103 which act on opposing elbows as shown in Figure 5, and Figure 7 is the force/time history for the combined force CF201. Figures 8 and 9 describe the subforces and combined force on a pipe leg which includes an area change.





Figure 6. Subforces SF101 and SF103 for the sample problem.



Figure 7. Combined force CF201 for the sample problem.



Force (N)

Figure 8. Subforces SF102, SF104 and SF106 for the sample problem.



Figure 9. Combined force CF202 for the sample problem.

6. COMPARISON WITH EXISTING TECHNIQUES

At EG&G Idaho, Inc., fluid induced forces have typically been approximated from RELAP5 hydrodynamic output by using only the pressure and momentum force terms applied at various points in the piping; this technique is documented in Reference 6 and will herein be referred to as the old approach. Recently, another technique to approximate the fluid induced forces was generated which utilized the pressure and momentum force terms in addition to a fluid acceleration term; this technique is documented in Reference 7 and will herein be referred to as the modified approach. This section provides a brief comparison between the old and modified approaches and the new approach used in the R5FORCE program. Refering to Figure 5, subforces SF105 and SF108, and the sum of these forces, CF203, will be used for the comparison. Two fluid transients were used, the sample problem discussed in Section 5 and the same sample problem with a liquid slug in the loop seal.

Evaluating the Section 5 sample problem first, Figures 10 and 11 provide time history information for subforces SF105 and SF108, respectively. Note that prior to and during the early stages of valve opening, the force predictions by the old, modified and new methods were very similar; as the fluid velocity became significant however, there were slight differences between the techniques. This was more evident in the time history of combined force CF203 which is shown in Figure 12. The modified and new methods predicted a peak force of approximately 7000 N (occurring immediately after the relief valve opened) which eventually approached zero as steady flow was achieved. The old approach predicted a higher maximum force of approximately 11,000 N which then decreased to a relatively constant value of 4000 N during steady flow. This significant force observed at steady state is not consistent with theory and is the result of neglecting the frictional shear force term. By computing the pressure and momentum forces at two points in a piping system, the momentum change between the two points is not balanced by the shear force, resulting in an unrealistic combined force. This was the only significant difference

observed between the old and the modified and new approaches. Differences between the modified and new method are slight, however, the new method will eliminate instabilities and data spikes previously encountered with the modified method, as shown in the next sample problem.

Evaluating the second sample problem, a liquic slug in the loop seal, igures 13, 14, and 15 provide time history information for subforces SF105 and SF108 and combined force CF203, respectively. The trends of this evaluation are identical to those noted is the first sample problem, except for data spikes associated with the modified method. The effect of these data spikes is clearly shown in Figure 16 for the modified method versus Figure 17 for the new method; combined force CF203 over the time range of 0.2 to 0.5 seconds. The old approach predicted a maximum force of approximately 47,000 N, decreasing to a relative constant value of 4,000 N during steady flow. The modified and new approaches are effectively identical except for the data spikes associated with the modified method. The new method predicted a peak force of approximately 41,000 N whereas the modified method, because of the data spikes, predicted a higher peak force of approximately 65,000 N. The modified method in this example would have resulted in peak forces approximately 60% higher than the new method, due entirely to data spikes. Other problems run with both methods have resulted in peak modified forces many orders of magnitude higher than the new method. In such situations, the user is required to examine the data in detail to eliminate potential data spikes, if possible.





Force (N)



NEW METHØD ØLD METHØD 13 MØDIFIED METHØD 2 4 X10 7.5 Figure 11. 5.0 Comparison of the old, modified and new approaches for subforce SF108 for the sample problem. (N) Force 2.5 0.0 3 -2.5 0.0 0.5 1.0

Time (s)

1.5

2.0

1

5



-

Time (s)



Force (N)

Figure 13. Comparison of the old, modified and new approaches for subforce SF105 for the second sample problem.


(N) sorof

Figure 14. Comparison of the old, modified and new approaches for subforce SF108 for the second sample problem.

Figure 15. Comparison of the old, modified and new approaches for combined force CF203 for the second sample problem.

amount of the old me

×



.

Time (s)

31



Force (N)





Force (N)

Figure 17. New approach for combined force CF 203 for the second sample problem from 0.2 to 0.5 seconds.

7. CONCLUSIONS

An approach has been outlined and a computer program developed for transient and steady state force calculations using hydrodynamic output data from the RELAP5/MOD1 computer code. This program is considered an improvement over existing force calculation techniques available at EG&G Idaho because it solves the force equation using the pressure and wall shear force terms instead of the pressure and fluid acceleration terms, eliminating potential instabilities associated with computing the time derivative in the fluid acceleration term; and uses output from the RELAP5/MOD1 program, an advanced one-dimensional computer program that is fast, accurate and easy to use.

It must be understood that verification studies with the R5FORCE program have been very limited and no comparison with experimental data has yet been made.

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APPENDIX A

DEVELOPMENT OF THE GENERAL FORCE EQUATION





APPENDIX A

DEVELOPMENT OF THE GENERAL FORCE EQUATION

A force can be exerted on a container in only three ways:

- 1. By means of pressure which acts on the surface of the container
- 2. By means of a shear force (friction) between a fluid and the surface of the container
- By means of an interaction between the container and a structural support member.

Consider the cross sectional view of the arbitrary shaped container shown in Figure A-1 where:

Sn	=	local normal stress
τ	*	local shear stress
ds		differential surface element
Ρ	-	local pressure
P	=	local density
u	=	local fluid velocity
ñ	-	unit vector normal to a surface
ñŢ	-	unit vector tangent to a surface
C		unit vector in the desired force direction
A		area





Figure A-1. Generalized fluid container.

A-2

with the following subscript notation:

I = internal
E = external
1 = control surface 1 (inlet)
2 = control surface 2 (outlet)

3 = control surface 3

The force acting on the control surface in the direction E can then be written as the sum of two surface integrals, or

$$F = \iint_{S} S_{n}(\bar{n} \cdot \bar{L}) ds + \iint_{S} \tau (\bar{n}_{T} \cdot \bar{L}) ds \qquad (A-1)$$

For an inviscid treatment, the shear term in Equation (A-1) is not used and the force is obtained utilizing only the normal force term. When viscous losses are considered, the shear force term in Equation (1) is generally difficult to evaluate. Through an application of the law of conservation of momentum, as alternate form of Equation (1) can be derived (footnote)^{*} and written in one-dimensional form as

$$F = -\frac{\partial}{\partial t} \iiint \frac{\dot{M}_{I}}{A_{I}} dV_{I} - (P_{I1} + P_{I1} U_{I1}^{2}) A_{I1} + (P_{I2} + P_{I2} U_{I2}^{2}) A_{I2}$$
(A-2)

R. L. Williamson, FORCE1: A Program to Compute Fluid Induced Forces Using Hydrodynamic Output from the RELAP5 Code, EGG-EA-5631, October 1981.



This technique is used extensively to evaluate fluid forces acting on a container. However, this technique has potential instabilities associated with computing the time derivative in the fluid acceleration term, often requiring various smoothing techniques to make the output useful.

If however, the shear force and pressure distribution are known for a container, Equation (A-1) can be used directly to obtain the fluid force on the container. Expanding Equation (A-1) over the three control surfaces identified in Figure A-1 and neglecting gravitational forces results in the following:

$$F = \iint_{CS1} S_{n_{11}} (\tilde{n}_{1} \cdot \tilde{L}) ds_{CS1} + \iint_{CS2} S_{n_{12}} (\tilde{n}_{2} \cdot \tilde{L}) ds_{CS2}$$

$$+ \iint_{CS3} S_{n_{13}} (\tilde{n}_{3} \cdot \tilde{L}) ds_{CS3} + \iint_{CS1} \tau_{11} (\tilde{n}_{T1} \cdot \tilde{L}) ds_{CS1}$$

$$+ \iint_{CS2} \tau_{12} (\tilde{n}_{T2} \cdot \tilde{L}) ds_{CS2} + \iint_{CS3} \tau_{13} (\tilde{n}_{T3} \cdot \tilde{L}) ds_{CS3}$$

$$- \iint_{CS1} S_{n_{E1}} (\tilde{n}_{1} \cdot \tilde{L}) ds_{CS1} - \iint_{CS2} S_{N_{E2}} (\tilde{n}_{2} \cdot \tilde{L}) ds_{CS2}$$

$$- \iint_{CS3} S_{n_{E3}} (\tilde{n}_{3} \cdot \tilde{L}) ds_{CS3} - \iint_{CS1} \tau_{E1} (\tilde{n}_{T1} \cdot \tilde{L}) ds_{CS1}$$

$$- \iint_{CS2} \tau_{E2} (\tilde{n}_{T2} \cdot \tilde{L}) ds_{CS2} - \iint_{CS3} \tau_{E3} (\tilde{n}_{T3} \cdot \tilde{L}) ds_{CS3}$$

Summing forces in the direction of fluid flow (\tilde{L}) and:

1. Neglecting external shear force effects, and

(A-2)

 Recognizing that for the one-dimensional uniform cross sectional area control volume assumption in RELAP5:

$$(\bar{n}_3 \cdot \bar{L}) = 0$$
$$(\bar{n}_{T1} \cdot \bar{L}) = 0$$
$$(\bar{n}_{T2} \cdot \bar{L}) = 0$$

Results in

 $F = \iint_{CS1} S_{n_{11}} (\tilde{n}_1 \cdot \tilde{L}) ds_{CS1} + \iint_{CS2} S_{n_{12}} (\tilde{n}_2 \cdot \tilde{L}) ds_{CS2}$ $+ \iint_{CS3} \tau_{13} (\tilde{n}_{T3} \cdot \tilde{L}) ds_{CS3} - \iint_{CS1} S_{n_{E1}} (\tilde{n}_1 \cdot \tilde{L}) ds_{CS1}$ $- \iint_{CS2} S_{n_{E2}} (\tilde{n}_2 \cdot \tilde{L}) ds_{CS2}$ (A-3)

Since the local static pressure distribution is not known, the normal stress will be defined in terms of the quasi steady change in momentum (the local static pressure plus the fluid momentum). In addition, the external fluid velocity effects will be neglected which is consistent with neglecting the external shear force effects, resulting in

$$F = \iint_{CS1} (P_{11} + \rho_1 u_1^2)(\bar{n}_1 \cdot \bar{L}) ds_{CS1}$$

+
$$\iint_{CS2} (P_{12} + \rho_1 u_1^2)(\bar{n}_2 \cdot \bar{L}) ds_{CS2}$$

+
$$\iint_{CS3} \tau_{13} (\tilde{n}_{T3} \cdot \tilde{L}) ds_{CS3} - \iint_{CS1} P_{E1} (\tilde{n}_1 \cdot \tilde{L}) ds_{CS1}$$

-
$$\iint_{CS2} P_{E2} (\tilde{n}_2 \cdot \tilde{L}) ds_{CS3}$$
(A-4)

Now, assuming that the fluid velocity, density and pressure are uniform over the local cross-sectional area and that the shear is uniform over the local control volume surface area, which is consistant with the one-dimensional approximation used in RELAP5, results in the following:

$$F = (P_{I1} + P_{I} u_{I}^{2})(\bar{n}_{1} \cdot \bar{L}) A_{I1} + (P_{I2} + P_{I} u_{I}^{2})(\bar{n}_{2} \cdot \bar{L}) A_{I2}$$

+ $\tau_{I3} (\bar{n}_{T3} \cdot \bar{L}) A_{I3} - P_{E1} (\bar{n}_{1} \cdot \bar{L}) A_{E1} - P_{E2} (\bar{n}_{2} \cdot \bar{L}) A_{E2}$ (A-5)

For the one-dimensional uniform cross-sectional area control volume assumption in RELAP5, the following unit vectors can be evaluated from Figure A-1:

$$(\bar{n}_{1} \cdot \bar{L}) = -1$$

 $(\bar{n}_{2} \cdot \bar{L}) = 1$
 $(\bar{n}_{13} \cdot \bar{L}) = 1$

Substituting these expressions into Equation (A-5) yields the following expression for the force acting on a container:



 $F = -(P_{11} + P_1 u_1^2)(A_{11}) + (P_{12} + P_1 u_1^2)(A_{12})$

+ * 13 A13 + PE1 AE1 - PE2 AE2

(A-6)



APPENDIX B

DEVELOPMENT OF THE JUNCTION PRESSURE AND JUNCTION AREA TERMS





APPENDIX B

DEVELOPMENT OF THE JUNCTION PRESSURE AND JUNCTION AREA TERMS

A general equation for the force exerted on a container has been developed and can be expressed as

 $F = -(P_{II} + P_{I} u_{I}^{2}) A_{II} + (P_{I2} + P_{I} u_{I}^{2}) A_{I2} + P_{EI} A_{EI} - P_{E2} A_{E2} + \tau A_{s} (B-1)$

where

Ø

τ

- A = volume surface area
- P = fluid pressure
- u = fluid velocity
 - = fluid density

= shear force per unit area

and the subscripts (I) and (E) refer to interior or external conditions, the subscripts (1) and (2) refer to the volume inlet or outlet and the subscript (s) refers to the interior surface area parallel to the flow.

Equation (B-1) is made up of five terms. Two of these terms represent forces associated with the volume inlet junction, two with the volume outlet junction and one with the volume itself. The application of Equation (B-1) will differ depending on the t_y pe of volume end geometry. In particular, a volume can be connected to an adjoining volume in one of four ways:



- Continued--Adjacent volumes are at the same angle, such as Volume: CV2 and CV3 in Figure B-1
- Bounded--Adjacent volumes are at different angles, such as Volumes CV3 and CV4 in Figure B-1
- Open--A volume represents the end of a pipe, although continued to an adjacent volume in the RELAP5 model, such as Volume CV4 in Figure B-1
- Special--Mechanistic junction models, such as the relief valve between Volumes CV1 and CV2 in Figure B-1.

These geometries can also contain area changes between adjacent volumes and a constant or variable junction throat ratio, simulating an orifice or a valve. The volume pressure and momentum, shear force and shear force area terms are readily available on the RELAP5 output tape. The internal and external quasi steady change in momentum at the inlet and outlet junction of each computational volume and the areas that the change in momentum acts on must be computed.

1. Development of the Junction Change in Momentum Term

The internal and external change in momentum (pressure plus momentum flux) at the inlet and outlet junction of each computational volume must be determined in order to determine the forces acting on that volume. The external pressure is defined through the input dawa and defaults to 14.7 psia (0.101 MPa) for all junction types except an open junction. For an open junction, the external pressure is defined as the pressure plus momentum flux in the adjacent downstream volume of the RELAP5 model. This will allow the effects of variable discharge conditions to be included in the analysis.

B-2



Figure B-1. Typical piping/control volume system.

The internal change in momentum is defined as the pressure plus momentum flux in a volume. The change in momentum at a junction must be approximated from the volume change in momentum. Only the outlet junction change in momentum will be developed for each junction type, the inlet junction change in momentum development being identical with the exception of the open junction which is not allowed as an inlet junction.

Continued Junction

Figure B-2 shows the location of the desired outlet junction change in momentum team. This quantity will be approximated using a ratio of the adjacent volume quantities and volume lengths as

$$(P + \rho U^{2})_{J} = \frac{(P + \rho U^{2})_{2} DL_{3} + (P + \rho U^{2})_{3} DL_{2}}{DL_{2} + DL_{3}}$$
(B-2)

This method will provide a reasonable approximation of the outlet junction change in momentum except for the following situations:

1. If the downstream volume (volume 3) is a time dependent volume, then DL_3 will be zero. For this situation, the computational and upstream volumes (volumes 1 and 2) will be used to approximate the outlet junction change in momentum as

$$(P + \rho U^{2})_{J} = (P + \rho U^{2})_{2} + \frac{DL_{2}}{DL_{1} + DL_{2}} \left[(P + \rho U^{2})_{2} - (P + \rho U^{2})_{1} \right]$$
(B-3)

2. If the outlet junction is choked or an area restriction (orifice, valve) exists at the junction, a non-linear decrease in the hydraulic head will occur and the adjacent change in momentum cannot be used to determine the outlet junction change in momentum. For this situation, the computational and upstream volumes (volumes 1 and 2) will be used to approximate the outlet junction change in momentum as discussed in item 1.



Figure B-2. Outlet junction change in momentum approximation method.

- 3. If either items 1 or 2 exist and if either the upstream volume (volume 1) is a time dependent volume (DL₁ will be zero) or the inlet junction is choked or an area restriction (orifice, valve) exists, the junction change in momentum will be set equal to the volume change in momentum.
- If a downstream volume does not exist, then the junction change in momentum will be set equal to the volume change in momentum.

Bounded Junction

The internal change in momentum for this type of junction is identical to the continued junction.

Open Junction

The internal change in momentum for an open junction will be determined by methods 2 and 3 for the continued junction. The other techniques are not applicable since there is no physical piping downstream of an open pipe (Volume 3 would not exist).

Special Junction

The internal change in momentum for this type of junction is identical to the continued junction.

2. Development of the Junction Area Term

The areas that the internal and external change in momentum acts on in each computational volume must be determined in order to determine the forces acting on that volume. Only the outlet junction area will be developed for each junction type, the inlet junction area development being identical with the exception of the open junction which is not allowed as an inlet junction. RELAP5 internal and output termnology will be used in the development of the following expressions.

Continued Junction

Figure B-3A shows the geometric configuration of a typical continued junction. The internal area must account for the effects of an area change between adjacent volumes and a junction flow area which could be larger or smaller than the computational volume. The effects of these two geometries are accounted for as

$$A_{IR} = A_{V2} - \min \left[\begin{array}{c} A_{J2} & TR_{J2} \\ A_{V3} \end{array} \right]$$
(B-6)

A zero or negative result means that there will be no area for the junction change in momentum to act on, thus there will be no force at that location.

The external area must account for the effects of an area change between adjacent volumes. The effect of this geometry is accounted for as

$$A_{ER} = A_{V2} - A_{V3}$$
 (B-7)

Bounded Junction

Figure B-3B shows the geometric configuration of a typical bounded junction. The internal area must account for the effects of an area change between the volume and the junction (A_{IR1}) as well as the area of the junction (A_{IR2}) . The effects of these two geometries are accounted for as

$$A_{1R} = A_{V1} - A_{11} * TR_{11}$$
(B-8)

 $A_{IR2} = A_{JI} * TR_{JI}$ (B-9)







Figure B-38. Bounded junction geometric configuration.





Figure B-3D. Special relief valve geometric configuration with the orifice on the valve outlet.

The external area must account for the effects of an area change between the computational volume and the junction as well as the bend. These geometries are accounted for as

$$A_{ER} = A_{V1}$$

Open Junction

Figure B-3C shows the geometric configuration of a typical open junction. The internal area must account for the effects of a junction flow area which could be larger or smaller than the computational volume. The effect of this geometry is accounted for as

$$A_{IR} = A_{V2} - A_{J2} * TR_{J2}$$
 (B-11)

The external area must account for the effects of a junction flow area which could be larger or smaller than the computational volume. The effect of this geometry is accounted for as

$$A_{FP} = A_{V2} - A_{12} * TR_{12}$$
(B-12)

Special Junction

Figure B-3D shows the geometric configuration of the special relief valve mechanistic model with the orifice on the valve outlet. The mechanistic model with the orifice on the valve inlet can be obtained by interchanging the inlet and outlet junction areas. The internal area must account for the effects of a dead end for one junction and a bounded junction for the other. The effects of these two geometries are accounted for as

$$A_{IR} = A_{VI}$$

(B-13)



(B-10)

$$A_{IL1} = A_{V2} - A_{J1} * TR_{J1}$$
 (B-14)

$$A_{IL2} = A_{J1} * TR_{J1}$$
 (B-15)

The external area must account for the effects of a bend. This geometry is accounted for as

$$A_{ER} = A_{V1}$$

(B-16)

 $A_{EL} = A_{V2}$







APPENDIX C

DEVELOPMENT OF THE SHEAR FORCE COMPONENT AND MODIFICATION OF THE RELAP5 ROUGHNESS TERM





APPENDIX C

DEVELOPMENT OF THE SHEAR FORCE COMPONENT AND MODIFICATION OF THE RELAPS ROUGHNESS TERM

1. DEVELOPMENT OF THE SHEAR FORCE COMPONENT

The force component attribution to shear can be considered to be the sum of the shear forces for the gas and fluid, or

$$F_{shear} = F_{shear_g} + F_{shear_f}$$
 (C-1)

where the shear force for each phase is equal to the shearing stress, or the wall friction per unit area for the phase times the pipe surface area proportional to the phase, or

$$F_{shear_g} = (\tau_g) (\alpha_g) (\pi D L)$$
(C-2)

 $F_{shear_{f}} = (\tau_{f}) (\alpha_{f}) (\pi D L)$ (C-3)

Reference (1) defines the wall friction drag coefficient as one eighth of the phasic friction factor times the absolute velocity times the pipe perimeter proportional to the phase divided by the pipe cross sectional area and the phasic void fraction, or

$$FW_{g} = \frac{\lambda_{g}}{8} \frac{u_{g}}{A} \frac{PER_{g}}{\alpha_{g}}$$
(C-4)

$$FW_{f} = \frac{\lambda_{f} \quad u_{f} \quad PER_{f}}{8 \quad A \quad \alpha_{f}}$$
(C-5)

The pipe perimeter proportional to the phase can be expressed as the phasic void fraction times the pipe perimeter (4A/D), or

$$PER_{g} = (\alpha_{g})(PER) = \frac{4 A \alpha_{g}}{D}$$
(C-6)

$$PER_{f} = (\alpha_{f})(PER) = \frac{4 A \alpha_{f}}{D}$$
(C-7)

Substituting the above into Equations (C-4) and (C-5) and solving for λ_{f} and λ_{g} yields

$$\lambda_{g} = \frac{(FW_{g})(2D)}{u_{g}} .$$
 (C-8)

$$\lambda_{f} = \frac{(FW_{f})(2D)}{u_{f}}$$
(C-9)

The wall friction per unit area is defined as one eighth of the friction factor times the phasic density times the velocity times the absolute velocity, or

$$\tau_g = \frac{1}{8} \lambda_g p_g u_g u_g$$
 (C-10)

$$\tau_{f} = \frac{1}{8} \lambda_{f} p_{f} u_{f} u_{f}$$
(C-11)

Substituting Equations (C-8) and (C-9) into the above yields

$$\tau_{g} = \frac{FW_{g} D \rho_{g} u_{g}}{4}$$
(C-1')

$$\tau_{f} = \frac{FW_{f} D \rho_{i} d_{f}}{4}$$
(C-13)

Substituting the above into Equations (C-2) and (C-3) yields

$$F_{\text{shear}_g} = \frac{FW_g D^2 \rho_g u_g \alpha_g \pi L}{4}$$
(C-14)

$$F_{\text{shear}_{f}} = \frac{FW_{f} D^{2} \rho_{f} u_{f} \alpha_{f} v L}{4}$$
(C-15)

2. MODIFICATION OF THE RELAPS ROUGHNESS TERM

Due to the solution technique used in R5FORCE, system components which result in a frictional loss, such as elbows, must be modeled by modifing the volume roughness rather than by adding a form loss coefficient at a junction. Form losses, such as orifices and valves, must still be calculated by the addition of an energy loss coefficient or an area change at a junction. This section of the appendix discusses how to modify the volume roughness term to account for frictional losses.

Currently, frictional loss geometries such as elbows are modeled by adding an energy loss coefficient at a junction. This energy loss coefficient is the product of the turbulent friction factor and the L-over-D ratio, or

$$K = f_{+} (L/D)_{1}$$
 (C-16)

where f, is based on the Colebrook Equation,

 $\sqrt{\frac{1}{f}} = -2 \log_{10} \left[\frac{E}{3.7 \text{ D}} + \frac{2.51}{R_{e}\sqrt{f}} \right]$ (C-17)



Assuming tubulent flow (R_e = large), this expression can be simplified to

$$\frac{1}{f_{t}} = -2 \log_{10} \frac{E}{3.7 D}$$

or,

$$f_{t} = \left[\frac{1}{-2 \log_{10} \frac{E}{3.7 D}}\right]^{2}$$
(C-18)

To modify the volume roughness, an equivalent turbulent friction factor must be determined as the sum of the above $f_t (L/D)_L$ and the $f_t (L/D)_v$ of the volume being modified, or

$$f_e (L/D)_v = f_t (L/D)_v + f_t (L/D)_L$$

or,

$$f_e = f_t \frac{(L/D)_v + (L/D)_L}{(L/D)_v}$$
 (C-19)

The equivalent turbulent friction factor can now be used to calculate an equivalent volume roughness by rearranging Equation (C-18) as

$$E_e = 3.7 \text{ D } 10 -2 \sqrt{f_e}$$
 (C-20)

Using this value [Equation (C-20)] of volume roughness instead of the normal pipe roughness will incorporate the effects of frictional losses into the shear term.

An an example, consider an elbow in a RELAP5 model which has an L-over-D loss of 16 (K = 16 f_t). The length and diameter of the volume

upstream of the elbow is 1.60 ft and 0.6651 ft (L/D = 2.406), and downstream of the elbow is 2.00 ft and 0.6651 ft (L/D = 3.007). The pipe roughness (E) is nominally 0.00015 ft.

Half the elbow resistance (L/D = 8) will be added to the volume upstream of the elbow and half downstream of the elbow. From Equation (C-18), the turbulent friction factor can be calculated for both volumes as,

$$f_t = \frac{1}{-2 \log_{10} \frac{0.00015}{(3.7)(0.6651)}}$$

 $f_t = 0.01407$

The equivalent turbulent friction factor can now be determined from Equation (C-19) as,

$$f_e (upstream) = 0.01407 \frac{2.406 + 8}{2.406}$$

= 0.0614

 $f_e (downstream) = 0.01407 \frac{3.007 + 8}{3.007}$

The equivalent volume roughness can now be calculated using Equation (C-20) as,

$$E_{\text{(upstream)}} = (3.7)(0.6651) 10 \frac{1}{-2\sqrt{0.0614}}$$

= 0.02314



 E_e (downstream) = (3.7)(0.6651) 10 -2 $\sqrt{0.0520}$

= 0.01542

Using these ${\rm E}_{\rm e}$ values for the respective volume roughness terms will simulate the effects of an elbow.



APPENDIX D

RELAP5 CODE UPDATES AND OUTPUT TAPE FORMAT





APPENDIX D

```
RELAPS CODE UPDATES AND OUTPUT TAPE FORMAT
```

```
1. RELAPS CODE UPDATES
*IDENT JCWTEST 1. RELAP5 CODE UPDATES
*DELETE RELAP5.6
* TAPE6=OUTPUT, DEBJG=OUTPUT, PLOTFL, STH2XT, TAPE23)
*BEFORE MOVER.56
                       *********************
00000000
   *** UPDATES TO WRITE A JCW STRESS
*** AT EVERY SUCCESSFUL TIMESTEP
*** (WRITES TO TAPE 23)
                                                         TAPE
                                                                    ***
                                                                    ***
                                                                     ***
   ************
                               JCW TAPE
         DATA JFLAG/0/
IF(JFLAG.NE.0) GD TD 85
JFLAG. = 1
CCC
      WRITE TOTAL NUMBER OF VOLUMES AND JUNCTIONS
   -
         NVOLUMS = 1 + (IVE - IV)/(IVSKP)
NJUNCTS = 1 + (IJE - IJ)/(IJSKP)
WRITE(23) NVOLUMS,NJUNCTS
COC
      COMPUTE AND WRITE CONTROL VOLUME GEOMETRY
         DD 83 I=IV, IVE, IVSKP
IF(DL(I).EQ.0.0)DZDL = 3.0
IF(DL(I).NE.0.0)DZDL = DZ(I)/(DL(I)*4.903325)
WRITE(23) VOLNO(I), AVOL(I), DZDL, DL(I)
    83
CCC
   - WRITE CONNECTION AND
                                       CONTROL PARAMETERS FOR JUNCTIONS
         DO 84 I=IJ, IJE, IJSKP
WRITE(23) JUNNO(I), AJUN(I), IJ1(I), IJ2(I)
    84
000
     WRITE THE PROBLEM TIME
    85 WRIFE(23) TIMEHY
CCC
     LOOP THROUGH CONTROL VOLUMES
         DO 86 ISTV, IVE, IVSKP
CCCC
      COMPUTE AVERAGE VOLUME SHEAR FORCE AND VOLUME PV**2 TERM
         PIE=3.1415927
FRF=FWALF(I)*VELF(I)*VOIDF(I)*DL(I)*PIE*DIAMV(I)**2*RHOF(I)*0.25
FRG=FWALG(I)*VELG(I)*VOIDG(I)*DL(I)*PIE*DIAMV(I)**2*RHOG(I)*0.25
FRTOT=FRF+FRG
         PV2V=V0IDF(I)*RH0F(I)*VELF(I)**2+
V0IDG(I)*RH0G(I)*VELG(I)**2
        3
ĉ
  - WRITE VOLUME INFORMATION TO TAPE
C
    86 WRITE(23) P(I), FRIDT, PV2V
CCC
   - LOOP THROUGH JUNCTIONS
         UO 87 I=IJ, IJE, IJSKP
CCC
     COMPUTE JUNCTION PV**2 TERM
   -
         PV2J=0.0
IF(ATHROT(I).GT.C.O) PV2J=
VOIDFJ(I)*RHOFJ(I)*(VELFJ(I)/ATHROT(I))**2*
VOIDGJ(I)*RHOGJ(I)*(VELGJ(I)/ATHROT(I))**2
        3
        8
Carse
     WRITE JUNCTION INFORMATION TO TAPE
    87 WRITE(23) ATHROT(I), PV2J, IJ2(I)
```

2. OUTPUT TAPE FORMAT

System Geometry (written once).

- 1. Total Number of Volumes; Total Number of Junctions
- For each volume, <u>Volume Number</u>; <u>Volume Area</u>; <u>Volume Inclination</u>; Volume Length
- For each junction, <u>Junction Number</u>; <u>Junction Area</u>; "From" Junction Control Flag; "To" Junction Control Flag.

Output Data (written every time step)

.

1. Time

- For each volume, <u>Volume Pressure</u>; <u>Average Volume Shear Force</u>; Average Volume Momentum Flux
- For each junction, <u>Junction Throat Ratio</u>; <u>Average Junction</u> <u>Momentum Flux</u>, <u>"To" Junction Control Flag</u> (Contains "To" Junction Choking Flag).


APPENDIX E

R5FORCE PROGRAM LISTING (MICROFILM)







R5FORCE PROGRAM LISTING











APPENDIX F



APPENDIX F

PROGRAM USERS GUIDE

The purpose of this appendix is to provide sufficient information to permit application of the R5FORCE program to a typical piping system. Included are a description of the force modeling strategy, detailed user input instructions, and a sample problem. It is recommended that the main body of this report be read and understood prior to using the program.

1. FORCE MODELING STRATEGY

The RELAP5 code numerically computes the fluid transient response within a piping system by dividing the system into a number of hydrodynamic control volumes connected by junctions. Associated with each control volume and junction is a nine digit integer reference number. This reference number is written to the RELAP5 hydrodynamic output tape and is therefore available for use in the force calculation program. In the R5FORCE input instructions, force control volumes can then be constructed simply by specifying the applicable RELAP5 control volume reference numbers.

F-1

2. R5FORCE INPUT AND OUTPUT

This section provides detailed input instructions and a discussion of the various modeling rules and sign conventions used in the R5FORCE program.

2.1 Input Instructions

All input data is in free format input and default information is contained in parenthesis. Input data need not be entered if default values are aceptable.

ard Number	PARAMETER
- 15	Title Card, with the "=" sign in Column 1
100	Output Units, "BRITISH" or "METRIC" (BRITISH)
	Input Units, "BRITISH" or "METRIC" (BRITISH)
200	Time Between Printouts, seconds (1.0)
	Start Time, seconds (0.0)
	Finish Time, seconds (1.0 x 10 ¹²)
300	Ambient Pressure, psia or Pa (14.7 psia or 0.101 MPa)
400	Type of Printed Output:
	Output contains problem definition and summary output in addition to the following options:
	"CHECK"input check only, problem stops at the end of input processing
	"NONE" no output at requested printout times
	"FORCES"Subforce and combined force output at requested printout times
	"ALL"Subforce, combined force and volume force output at requested printout times
	(FORCES)
500	Maximum Number of Subforces Per Combined Force (5)

- Junction number of bends when both adjacent volumes are horizontal (more than one junction number can be on a card)
- 620 Junction number of a special geometry, such as a relief valve, with an orifice at the outlet but not at the inlet. This geometry assumes the adjacent volumes are at angles to each other. (More than one junction number can be on a card)
- 640 Same as the 620 card except the orifice is at the inlet only, not the outlet.
- 700 Initial force zeroing "NONZERO"--Do not zero initial forces
- 1XXX Subforce input information for all geometries except an open pipe (XXX is the subforce number)

Direction of subforce relative to the RELAP5 model. A positive number is in the direction of positive flow in the RELAP5 model and a negative number is in the direction of negative flow in the RELAP5 model.

Beginning control volume number of the subforce relative to the RELAP5 model

Ending control volume number of the subforce relative to the RELAP5 model. If this control volume number is the same as the beginning control volume number, either a zero may be entered or the control volume number may be repeated.

Combined Force Number/Direction relative to subforce direction. A positive number is in the direction of the subforce and a negative number is in the opposite direction of the subforce. Note that a combined force number need not be entered.

2XXX

600

Subforce input information for an open pipe. Input identical to card !XXX.

2.2 Force Direction Conventions

In order to be consistent with the basic equations solved in R5FORCE, the following conventions must be followed.

 The RELAP5 model must be developed in the direction of positive flow.

- The force direction must be colinear with the pipe axis, in any direction.
- System components which result in a frictional loss, such as elbows, must be modeled by modifing the volume roughness rather than by adding an energy loss coefficient at a junction.
- Branch components in RELAP5 cannot be included in the definition of a subforce or a combined force.

2.3. Output

The R5FORCE program writes information to both an output file (which is usually printed) and a disk or tape file (for structural input).

The output file contains an echo of all input data, information about input data processing, and then force results at requested printout times. This information is considered self-explanatory and will be shown in a sample problem to be discussed later.

Two disk or tape files are currently written at every time step in the following format:

- (1) TIME, FORCE 1, FORCE 2,, FORCE N,
- (2) TIME, PRESSURE 1, PRESSURE 2,, PRESSURE M,

where N is the total number of subforces and combined forces and M is the total number of RELAP5 hydrodynamic control volumes. The force file is called TAPE13. In addition, a plotting file called OOSCRA is generated which contains force versus time information in a Common Word Addressable File (CWAF) formated data file. The last page of input processing (in the previously discussed output file) provides a description of the time/force array. For reference purposes, the total number of time steps on the disk or tape file is also written on the output file following the last time step. Also written out is a summary of the maximum positive and negative volume forces, subforces and combined forces.

3. SAMPLE PROBLEM

A detailed sample problem is now presented to help users become familiar with the use of the R5FORCE program.

The piping system geometry and fluid transient used for the sample problem have been previously described in the main body of this report. Figure F-1 thows the piping system and includes a description of the subforces and combined forces to be computed. Figure F-2 is a RELAP5 nodalization diagram of this system showing the hydrodynamic control volumes and junctions as well as each of the control volumes used for force calculations. Note that in general, a force control volume is made up of several hydrodynamic control volumes. A description of the required RSFORCE input data for this sample problem is listed in Figure F-3.

Prior to performing any calculations the R5FORCE program provides an echo of the input data (Figure F-3), and then processes this data. During processing, the user is provided with a description of the RELAP5 hydrodynamic model, information on each of the component and combined forces, a description of the output format of the force file, the initial forces in the system at time zero and the resultant zeroed forces at time zero. Note that all later force values are in reference to the zeroed force values. Appendix G contains a copy of this input processing description for the sample problem.

Figures F-4, F-5, and F-6 represent sample force results at times 0.1, 0.25, and 0.7 s, respectfully. At 0.1 s, the relief valve is completely closed and the only significant unbalanced force (see the combined forces in Figure F-4) occurs upstream of the relief valve which is undergoing rapid pressurization. At 0.25 s the relief valve is in the process of opening and there exists significant unbalanced forces at all points in the system. At 0.7 s the flow is essentially at steady-state and the unbalanced forces are small.





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Figure F-2. RELAP5 nodalization diagram of sample piping system.



FORCE-TIME HISTORY FROM RELAPS OUTPUT DATA - VOLUME FORCE DATA

SAMPLE PROBLEM - RELIEF VALVE DISCHARGE W/O LCOP SEAL

PREBLEM TIME = 1.0000-01 LATA SET NUMBER = 21

INLET EXT. FORCE UUTLET EXT. INLET INT. CUTLET INT. TOTAL FORCE FURCE FORCE (NENTONS) SHEAR FORCE FCRCE (NEWTENS) VOL. NLM. (NENTENS) (NENTONS) -INERTENS) (NENTONS) gur -3.2420EE+C5 6. -3.242CEF+05 C . 101010000 1.14177E+C5 1.5100eE-C2 (m) C . 15092 1.51006E-02 1.91061E-02 3.14350E-02 0. 3.141776+05 103010000 20101000 20102000 20102000 20102000 0. 6. 0. C. \$7998.2 6. 7995.2 40 0. \$ 0. -4635.8 4t38.4 C . -4638.3 3.1432CCU-C22 1.432CCU-C23 1.432CCU-C23 3.1432CCU-C23 3.1452CU-C23 1.452CU-C23 0. -4138.4 6. 6. 201040000 4641.5 4641.5 U. 201050000 20106000 20107000 201080000 201080000 201080000 0.-4641.5 C . -2.3025 0. 70 4639.1 6. RSFORCE -4639.1 C . 4. G . . -4639.1 9.12936E-64 0. 0. 6. U = ---4616.8 4618.8 U. 6.0 0. .73835 .73835 G. 6.0 -1.252868-67 -2.157688-67 -3.624468-67 100 203010000 G . C . C . 0. 203020000 6. Ú. -0. 6. 203030000 é 4. 6. 6. 0. in -.73175 -.73175 C . 0. E 4. 0. -2.675145-07 -3.223132-07 -2.897572-07 -3.680505-07 .7317: 6. 6. 203060000 -3.22313E-C7 0. ts 0. 6. 203070000 U. -3.6805LE-C7 C. 0. . £600P Ú. 000000000000000 0. C 0. a -3.68C5CE-07 -4.46226E-C7 -6.61768E-C7 -6.61768E-C7 -6.61768E-C7 -7.5676E-C7 -8.34863E-C7 -4.466256-67 0. C . -5.2528CE-C7 1 6. 0. 203100000 U. 6. 6. ¥ ... 0 203110000 0. 20312000 20313000 20314000 20315000 20315000 6. 0. -1.817861-C7 C . C . G . 0. -4. -7.585762-67 6. C . 6. -6.34883E-C7 -9.09012E-C7 6. S 0. 6. 0. C -9.600126-07 -9.600116-07 -1.053865-06 -1.122.66-06 0. 0. 0. 0. -9.ECELIE-CI 6. 0. C . 20317000 6. -1.0530cE-Ce 6. 0. 0. 6. .58939 0. C . 63196600 0. -1.305476-00 -1.4053160-00 -1.4031000-00 -1.531000-00 -1.723010-00 -. 58939 0. 6. C . 203200000 -1.46236E-Ct 0. 6. G . 203210000 C . -1.6313LE-CE -1.69252E-CE -1.72381E-CE 20323CCC0 20323CC00 20324CC00 20325CC00 20325CC00 20325CC00 C . C . C . 0. 6. U . 0. Q . 0. 6. 6. 0. -1.7t9t51-Ct -1.76985F-06 1. 0. 0. 11 . .36317 .36318 0. -1.49297F-C6 6. 0. -.36318 0. -.36318 0. 6. 20327000 -1. CC1SE-CE 2.328311-CE 6. 6. -1.+CC19E-C6 G . 0. 1.26894E-C7 v. -3.C3611E-07 C . C .

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FERCE-TIME & TERY FROM RELAPS OUTPUT DATA - SUBFORCE AND COMBINED FORCE DATA

SAMPLE PRO - PELIEF VALVE DISCHARCE NO LCCP SEAL

PREBLER TIR COCE-01 DATA SET NUMBER = 21

FORCE	NEATLAS CE	INLET INT. FORCE (NEATONS)	GUTLET INT. FORCE (NEWTOWS)	INLET EXT. FORCE (NEWTONS)	OUTLET EXT. FONCE (NEWTONS)	TOTAL FORCE (NENTONS)
SF1022 SF1004 SF11004 SF11004 SF11007 SF11007 SF11007 SF12002 SF12002 SF12002 SF1002 S	4.3007136-007 -1.20176-007 -1.20176-006 -2.30176-006 -2.30176-006 -2.30176-006 -2.30176-006 -2.30176-006 -2.30176-006 -2.30176-006 -2.30176-006 -2.30176-006 -1.501776-006 -1.501776-006 -1.501776-006 -1.501776-006 -1.501776-006 -1.501776-006 -1.501776-006	73835 73175 	0. 0. 0. 58939 0. 36318 73175 58939 .36318 3175 .58939 .36318		C. O. C. C. C. C. C. C. C. C. C. C. C. C. C.	73175 73175 66006 56936 36318 36317 6.60406E-03 1.5012 22622
			anne a tha an tha an the second and a second a			
			The Association Station of the Stationary Solid Stationary			
S. A.			a a a cara a			
	46					

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FERCE-TIME HISTERY FROM RELAPS CUTPUT DATA - VOLUME FORCE DATA

SAMPLE PROBLEP - RELIEF VALVE SISCHARGE +10 LCOP SEAL

LATA SET NUMBER . 110 PECBLEM TIME = .250

atora to a

* 0

T	VOL. NUP.	SHEAR FORCE	INLET INT. FORCE (NENTONS)	OUTLET INT. FORCE (NEWTONS)	INLET EXT. FORCE (NEWTONS)	OUTLET EXT. FORCE (NEWTONS)	TOTAL FERCE (NEWTONS)	
igure	101010000	C. 7649	-8.10585E+05	0. 7.92193E+05	с. с.	0. 0. 0.	- E . 1 C589E + C5 7.52195E + C5 55.903 1.93532E + C4	
F-5.	20103CC0C 20104CC03 20105CC00 20105CC00 20106CC00	2020	-1.232165+04 -1.125156+04 -9652.0	1.12919E+C4 9852.6 9246.6	0. C. C.		-723.24 -1.1C854E+C4 1.CC609E+C4 -25C.84 -9C41.3	
R5FORCE	201050000 201050000 20301000 20302000	113.62 123.29 111.e1 357.13	-6.34095E+04 C.	6. 8413.0 0.		0. 0. 0.	113.82 8546.3 -6.32983E+C4 357.13 436.44	
resul	20303000 20304000 20305000 20305000 20305000 20305000	436.44 474.26 1036.6 321.37	0. 0. -2.94794E+C4	5.94794E+04 C.	00000	0.	474.26 6.064866.04 -5.644246.04 321.37 -2.410696.04	
ts at	2C3C8CC00 2C3O9CC00 2C31CCC0C 2C311CCCC 2C311CCCC	169.78 235.61 255.17 255.15 275.00	-2.427668+04 U. U. U. U. U.			с. о.	235.61 259.17 266.15 27C.CC	
0.25 s	203130000 20314000 20315000 20316000	267.64	0. 0. 0.	0. 	C. 	 	261.62 243.61	
	20318CC00 20319CC00 2032CCCC0 2032CCCC0	236.67 1602.67	0. -3.66907E+04	3.66907E+04	C . O . O .	0. 0. 0.	236.69 3.76813E+C4 -3.56881E+C4 255.61 254.75	
	20322000 20323000 20324000 20325000 20325000	254 - 19 2558 - 25 2550 - 27 900 - 55	C.	0. 2.75479E+04			251.82 258.25 256.27 2.64546E+C4	
	2C328CC00 2C528CC00 2C5C1CC00	Pel.51 253.95 0.	-2.75479E+04 0. -#65.28	432.06	C. C.	č.	253.95 65.785	

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FERCE-TIME HISTORY FROM RELAPS OUTPUT DATA - SUBFORCE AND COMBINED FORCE DATA

SAMPLE PROBLEM - RELIEF VALVE DISCHARGE MIG LCCP SEAL

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PACALE	M TIME250	CATA SE	T NUMPER = 110			
FORCE	SHEAR FORCE (NEWTONS)	INLET INT. FORCE (NEWTONS)	OUTLET INT. FORCE (NENTONS)	INLET EXT. FORCE (NEWTONS)	OUTLET EXT. FORCE (NEWTONS)	TOTAL FORCE
5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	-111:61 -13:7.0 -2487.00 -165.7.78 -165.7.78 -115435.5 -11177.8 -21778.60 -21778.60 -5071.02	6.34095E.04 5.94794E.04 0. 2.42766E.04 3.66907E.04 0. 2.75475E.04 0. -6.34099E.04 -8.37561E.04 -3.66907E.04	0. 5.94794E+C4 0. 3.t6907E+04 2.75479E+04 5.94794E+04 3.t6907E+04 3.t6907E+04 2.75479E+04	· · · · · · · · · · · · · · · · · · ·		E.32983E*C4 5.61215E*C4 E.19665E*C4 3.56b81E*C4 4.6234CE*C4 2.64324E*C4 2.64324E*C4 2.64324E*C4 -1.331.6 -4.19944E*C4 -5562.6
n						

FERCE-TIPE HISTORY FROM RELAPS OUTPUT LATA - VOLUME FORCE UATA SAMPLE PROELEM - RELIEF VALVE LISCHARGE NO LOUP SEAL

ACCOUNT TIME - TO LATA SET NUMBER = 830

 1 12 4	3 5 4	0 3		
	174			
 L 188		~ ~		

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VOL. NUM.	SHEAR FORCE	INLET INT. FORCE (NEWTONS)	GUTLET INT. FORCE (NEATONS)	INLEI EXT. FORCE (NEWTONS)	FORCE INENTONSI	TOTAL FORCE (NENTONS)
10101000	0:	-1.620916+06	0. 1.5.1551+06	¢:	ŭ. 5.	-1.62091E+C6 1.58156E+C6
2C101CCC0 2C102CC00 2C102CC00	56.768 126.08 314.61	0. -2.514921+04	4.12556E+64 2.48453E+04	C. C.	0.	4.13816E+C4 1C+652 -2.4636EE+C4
20104CC00 20105CC00 20106CC00 20107C000	202.45 316.12 208.28	-2.48453E+04 -2.43725E+64 -2.46663E+64	2.43725E+04 2.4C6ale+04 G.	¢.	0.	2.4581/[+C4 11.68 ~2.32590E+C4
201080000 201090000 203010000	117.52 146.73 169.40 347.87	-7.40630E+04	2.35310E+04	¢.	0.	2.26717E+C4 -7.29535E+C4 347.87
203030000 203040000 203050000	427.00 473.00 1265.00	-7.C4152E+04	0. 7.C4152E+04		0.	472.68 7.16864E+C4 -6.92947E+C4
203070000 203080000 + 203090000	361.53 200.69 243.13	-3.7100EE+04	0. 0. 0.			-3.68999E+C4 243.13 258.05
203110000 20312000 20312000	269.17			¢. ¢.	0. 0. 0.	265.03 265.17 272.41 274.84
2C315CC30 2C316CC60 2C317CC00	277.3E 279.69 282.48	C	Ŭ. U.	ç.	0.	277.36 275.89 262.48 265.16
2C318CC00 2C319CC00 2C32CCC00 2C321CC00	1240.52	-6.94259E+04	6.94259E+04	č.		7.CC8LCE+C4 -6.EC855E+C4 355.C2 367.55
20323000 20323000 20324000 20325000 20326000	3677-859 377-859 405-54 416-40 1623-9		6.58143E+04			377.65 405.94 416.40 6.743016+04 -6.414596+04
20327000	575.37	-571.27	637.44	c.	č:	575.37 66.164

FURCE-TIME HISTORY FROM RELAPS CUTPLE CATA - SUBFORCE AND COMBINED FORCE DATA

SAMPLE PROPLET - RELIEF VALVE DISCHARCE NO LEOP SEAL

PREBLEM TIME = .700 CATA SET NUMBER . 830

- Fi	FORCE	SHEAR FERCE	INLET INT. FORCE (NENTURS)	GUTLET INT. FORCE (NEWTONS)	INLET EXT. FORCE (NEWTONS)	OUTLET EXT. FURCE (NEWTONS)	TUTAL FCKCE (NENTONS)
gure F-	SF101 SF102 SF103 SF104	-105.50 -1452.0 -2514.0 -200.69	7.406361.04 7.641521.04 3.710011.04	0. 7.c4152€+04	0: 	0. C. C.	7.34535E+C4 E.E9332E+C4 7.29292E+C4 3.66995E+C4 F.RC455E+C4
6 (Contd.)	SF100 SF100 SF100 SF100 CF200 CF200	- 13574407.54 - 23574407.55 - 23574407.51 - 23574407.51 - 2357440507.1		0.54259E+04 0.52143E+04 7.64152E+04 0.52152E+04 0.52143E+04	··· ··· ··· ···	0. 0. 0. 0.	7.33934E+C4 E.35705E+C4 E.35705E+C4 -1C24.3 -3.24397E+C4 1275.5
R5FORCE						n anna a seann ann ann an an an	
results							
at 0.7 s							
				27 mars 100 m			
.7 s.							

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Upon completion of the requested force calculations, the R5FORCE program provides a summary identifying the maximum positive and negative forces encountered for each volume force, subforce and combined force requested, including the time of the maximum force. Appendix H contains a copy of this output for the sample problem.



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APPENDIX G

SAMPLE PROBLEM INPUT PROCESSING DESCRIPTION





FCRCE-TIME SAMPLE PR	HISTORY FROM R OPLEM - RELIEF	VALVE DISCHARGE .	- INPUT DESCRIPTIO	ERGN JUN. TYPE	10/15/82	12.03.20
101 102 103 104 105 106 107 106	-1 -1 +1 -1 +1 -1 +1 +1 +1	20301CC0C 20306CC0C 20306-760 20326C0C 20326C0C 20327CC0C 20321CC0C	203010000 203070000 20305000 20326000 20320000 20320000 203260000 203260000	ECUNCED BCUNDED BCUNDED	BCUNDED BCUNDED GPEN BCUNDED	-201 -202 *201 -202 -202 -203 *202 *203
<u>.</u>						
			2000 - 100 - 100 1000 - 100 1000 - 100			
						- 1 miles

	Saure	e reduce.					NETTEN INFORMAT	TICN	TC JLN	CTION INFORMAT	ION
T	VOL. NUP.	LENGTH	AREA (SQ. PETERS)	FRCP VCL.	TO VOL.	NUMBER	ISC. METERS)	TYPE	NUMBER	(SO. PETERS)	
2 3 4 5 6	101C10CC0 103C10CC0 201C10CC0	C. 3.0114 .45720	.94031 .94031 2.35230E-02 2.35230E-02	101010000 103010000 201010000	103010000 201010000 201020000 201030000 201030000	1020CCCCC 1040CCCCCC 20101CCCC	.54031 2.35230E-02 2.5230E-02 1.36475E-02	BOUND	1C20CCCCC 1C46CCLCC 2C101CCCC 2C102CC0C 20103CCCC	.94031 2.35230E-02 2.35230E-02 1.36475E-02 1.36475E-02	ECUND
7 #	201030000 201040000 201050000	.45720 .38100 .38100	1.36475E-C2 1.36475E-O2 1.36475E-O2 1.36475E-O2	201020000	261050600 261050000 261050000 201070000	20103CCCC 20104CCCC 20105CCCC	1.36475E-02 1.36475E-02 1.36475E-02 1.36475E-02	BOUND BOUNC	201050000	1.36475E-C2 1.36475E-C2 1.36475E-C2	ECUND
10	201020000	-381CC -381C0 -4572C	1.36475E-02 1.36475E-C2 1.36475E-C2 1.36475E-C2	261060000 201070000 261080000 201090000	201050C0C 201090C0C 203010000 203020000	201070000	1.36475E-02 1.36475E-02 1.36475E-02		20102000000	1.36475E-62 3.22745E-62	ECUND
13	203020000 203020000 203030000 203040000	48768 48768 48768	3.22745E-02 3.22745E-02 3.22745E-02	203020000	2030306000 203050000 203050000	203020000	1.22745E-C2 1.22745E-C2 3.22745E-C2	Brubb	2030300000	3.22745E-C2 3.22745E-C2 3.22745E-C2 3.22745E-C2	ECUND
1.6	203050000 203060000 203070000 203080000	.48766 .30460 .30480 .45720	3.22745E-02 3.22745E-02 3.22745E-02 6.55716E-02	201050000	263676000	203040000	3.22745E-C2 3.22745E-C2 3.22745E-C2 6.55716E-C2	BUONE	203070000	3.22745E-C2 6.5571CE-C2 6.5571CE-C2 6.5571CE-C2	
18 10 20 21 22	203650660 203100660 203110660 203120660 203130660 203130660 203140660	45720 45720 45720 45720 45720 45720	6.55710E-02 6.55710E-02 6.55710E-02 6.55710E-02 6.55710E-02 6.55710E-02 6.55710E-02 6.55710E-02	2031090000 203100000 203110000 203120000 203120000 203120000 203120000	203116000 20312000 20313000 20314000 203150000 203160000 203160000	203056000 203106000 203126000 203126000 203126000 203146000 203146000	6.55710E-02 6.55710E-02 6.55710E-02 6.55710E-02 6.55710E-02 6.55710E-02 6.55710E-02		203120000 203120000 203120000 203130000 203140000 203140000 203140000	6.55710E-02 6.55710E-02 6.55710E-02 6.55710E-02 6.55710E-02 6.55710E-02	
23 24 25 26 26	203160CC0 203176CC0 203180CC0 203180CC0 203200CC0 203200CC0	4572C 4572C 4572C 5334C	6.55710E-C2 6.55710E-02 6.55710E-02 6.55710E-C2 6.55710E-C2 6.55710E-C2 6.55710E-C2	203146660 203176660 203186600 203186600 203196600 203260600	203130000 203190000 203200000 203210000 203220000 203220000	203120000 203120000 2031900000 2031900000 203200000 203200000	6.55710E-C2 6.55710E-C2 6.55710E-C2 6.55710E-C2 6.55710E-C2 6.55710E-C2	BOUND	203160000		EDUND
28 27 33 3 12	203230CC0 203230CC0 203250CC0 203250CC0 203250CC0 203270CC0 203270CC0 203270CC0	5334C 555870 555870 45720 45720	6.55710E-02 6.55710E-02 6.55710E-02 6.55710E-02 6.55710E-02 6.55710E-02 6.55710E-02	201210000 201210000 201210000 201210000 201210000 201210000 201210000 2012100000	203250000 203250000 203250000 203270000 203280000 205010000	203220000 203240000 203240000 203240000 203240000 203270000 203270000	t.55710t-C2 t.55710t-C2 t.55710t-C2 t.55710t-C2 t.55710t-C2 t.55710t-C2 t.55710t-C2 t.55710t-C2	BULNC	203250000 203250000 203250000 20326000 203270000 203270000	6.55710E-C2 6.5571CE-C2 6.5571CE-C2 6.5571CE-C2 6.5571CE-C2	E CUND CPEN

FORCE-TIME HISTORY FROM RELAPS CUTPUT DATA - DESCRIPTION OF RELAPS FYERCOYNAMIC VOLUMES AND JUNCTIONS SAMPLE PROBLEM - RELIEF VALVE DISCHARGE W/O LCCP SEAL . 10/15/82

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FORCE-TIME HISTORY FROM RELAPS GUTPUT DATA - INITIALIZED VOLUME FORCE CATA

SAMPLE PROBLEM - RELIEF VALVE DISCHARGE #/0 LCOP SEAL

10/15/82 12.03.20.

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VOL. NUM.	SHEAR FORCE	INLET INT. FORCE (NENTUNS)	CUTLET INT. FORCE INENTONS)	INLET EXT. FORCE (NEWTONS)	FORCE (NENTONS)	TOTAL FORCE (NENTONS)	
10101000	0.	-1.555985+07	0: 1:51705E+07	9.53C36E+C4	-9.29195E+04	-1.54645E+67	
20102000	0.	0. -2.25830E+05 -2.2583CE+05	3.89246E+05 2.25830E+05	C. 1363.2 1383.2	-2364.1 -1383.2 0.	3.86862E+C5 -2.24447E+C5	
20105000	C. O.	-2.2583CE+05 -2.2583CE+05	2.25830E+05 2.25830E+05 0.	1363.2	-1363.2 -1363.2 U.	2.24447E+05 -2.24447E+05	
A 201050000 A 201090000 20301000	0. 0. 0.	-3271.1	2.25830E+05	3271.1	-1383.2 0.	2.24447E+C5 -1.45515E-11 C.	
* 20304000 * 203040000 * 203050000 20306000		0. 0. -3271.1	9. 3271.1 9.		-3271.1	1.45519E-11 -1.45519E-11	
2C307CC00 2C309CC00 2C309CC00 2C309CCC0 2C31CCC00	C. 0.	-3374.7 G.	č. 0.	3374.7 0:		-1.45519E-11	
2C311CCCC 2C312CC00 2C312CC00 2C312CC00	0. 0. 0.	0. 0.	U. U. U. U.			с. с.	
* 20315000 20315000 20315000 20315000 20315000	C. C. C.		0. C. 0. 6645.8	с. с.	0. 0. -6645.8	C. C. 2.91030E-11	
203210000 203220000	6	-6645.8 C. U.	0. 	6645.8 C. C.	0. 0. 0.	-2.910302-11 C. C.	
20324000 20325000 20326000 20326000	с. с.	0. C. -£645.8	C. G. EE 95.8 C.	C. C. 6645.8	C. -0645.8 U.		
203280000	¢. ¢.	-0.751412+04	4.41600E+04	0.75141E+C4	-7.416001+04	č:	



FERCE-TIME HISTORY FROM RELAPS OUTPUT DATA - VOLUME FORCE DATA

SAMPLE PROBLEM - RELIEF VALVE DISCHARGE W/D LCCP SEAL

PRCOLEM TIME . 0.

CATA SET NUMBER = 1

VCL. NUM.	SHEAR FORCE	INLET INT. FCRCF (NEATONS)	FOPCE (NETTONS)	INLET EXT. FORCE (NEWTCNS)	OUTLET EXT. FORCE (NENTONS)	TOTAL FORCE (NEWTONS)
161616660	ç.	9.	0.	ç.	0.	£ : .
20101000	0. C.	0.	0.	¢.	0. 0. C.	ç.
201040000 201050000 201070000 201070000	 	 		· · · · · · · · · · · · · · · · · · ·	0.	· · · · · · · · · · · · · · · · · · ·
6 20108000 6 203010000 203020000	0. 0. 0.	0.	G. G. G.	C. C.	0. 0. 0.	
203040000 20305000 20305000	· · · · · · · · · · · · · · · · · · ·	0.	C. C.	0. 	0.0.0	c. c.
203080000 203090000 203100000	0.	0. 0.	C. U. Q.	0. 	C. U. U.	c. c.
20312000	0. 0. 0.	0. 	Ç. Ç.	0. C.	0. 0.	C. C.
2C316CCC0 2C317CCC0 2C318CCCC		0.	C. U.	Ç.	0. 0.	C. C.
2C320CCC0 2C321CC00 2C322CCC0	с. с.	0. 	с. 	с. с.	0. 	C.
20325000	C. O.	· · · · · · · · · · · · · · · · · · ·		¢.		
* 20327000 * 20328000 20501000	C.	u. 	č.	ç.	0.	č

12.03.20.

10/15/82

FORCE-TIME HISTORY FROM RELAPS CUIPUT DATA - SUBFORCE AND COMBINED FORCE DATA 10/15/82 12.03.20. SAMPLE PROBLEM - RELIEF VALVE DISCHARGE W/O LCOP SEAL 1 LATA SET NUMBER = PRCELEM TIME . 0. . OUTLET EXT. FORCE (NEWTONS) CUTLET INT. FORCE (NEWTONS) INLET EXT. FORCE INLET INT. FORCE (NEWIONS) FORCE NUMEER TOTAL FORCE SHEAR FORCE (NENTENS) 0. C . 6. 0. 0. 0. C. 0. с. 0. 0. 0. 0. C. C. C. C . Č. 6. ç. 0. Lin. C . 0. 0. -7 *









SAMPLE PROBLEM OUTPUT SUMMARY

APPENDIX H



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10/15/82 SAMPLE PROBLEM - RELIEF VALVE DISCHARGE NO LCOP SEAL

FORCE	SHEAR FERCE	INLET INT. FURCE (NENTONS)	CUTLET INT. FGRCE (NETIONS)	INLET EXT. FORCE (NEWTONS)	CUTLET EXT. FLPCE (NEWTENS)	FURCE (NENTONS)	FORCE (SECONDS)
	°1.2286	-1.62089£+06	1.71807E+07 1.59679E+06 C.	0.	č:	1.55598E+07 1.55679E+C6 67.772	1.CC -510 -257
201020000	127.49 8.6579 .97451	-2785.0 7349.3	4.1E364E+C4 5492.0 C.	0.	c. c. c.	4.19659E+C4 2715.6 735C.2 2.51C32E+C4	.510 1.43 1.44 .555
201060000 201070000 7 201060000	13.647 2.2667 116.66	-7283.7 1.1C1:5E+04 C.	9144+2 C. C. 2. 423855+04	0.00	č. č.	1874.2 1.10177E+C4 118.66 2.43FGGE+04	1.43
- 20301000 20302000 203030000	4.13412E-C3 363.46 441.15	1317.2 C:	C. C.	0		1317.2 363.4d 441.15	1.52
203C40CC0 203C5CCC0 203C6CCC0 203C6CCC0	1266.1 .34317 362.35	1220.6	7.05485E+04 C. C.			7.18146E+C4	1.01
203C80CC0 203C40CC6 2031CCCC0 203110CC0	264.26 294.56 311.11	C.	 c. c.	0.00.00.000	c. c.	264.20 294.56 311.11	
20312CCC0 203130CC0 203140CC0 203150CC0	32C.89 32t.55 329.3C 325.7C		· · · · · · · · · · · · · · · · · · ·	0.	C. C.	326.89	-273
203120CCC 203170CC0 20312CCCC	328.C2 324.40 318.98	Ç	C. C. 6.95467E+04	- 0: 0: 0:	· · · · · · · · · · · · · · · · · · ·	328.02 324.40 318.58 7.080836+64	·274 ·274 ·274 ·274
20320CCC0 20321CCC0 203220CC0	9.4679 363.39 368.76	1979.7 C:	с. с.	0.	· · · · · · · · · · · · · · · · · · ·	1969.6 363.39 365.76	·277 •279 •279
203240CC0 203250CC0 203260CC0 203260CC0	400.37	C. C.	C. 59C22E+04	0.00		406.37 416.76 6.75268t+04 444.76	.612 .614 1.62
203280000		C	C	J .	6.	575.64	.tlt

FERCE-TIME HISTERY FROM RELAPS OUTPUT DATA - SUMMARY OF MAXIMUM FOSITIVE VELUME FORCES

12.03.20.

FERCE-TIME HISTORY FROM RELAPS CUTPUT DATA - SUMMARY OF MAXIMUM NEGATIVE VOLUME FORCES

SAMPLE PROBLEM - RELIEF VALVE DISCHARGE NO LCCP SEAL

10/15/82

12.03.20.

FORCE	SHEAR FORCE	INLET INT. FORCE (NE.TONS)	CUTLET INT. FGRCE (NENTONS)	INLET EXT. FORCE (NEWTONS)	GUTLET EXT.	FCRCE (NEWTONS)	TIME OF MAXIMUP FURCE (SECONDS)
101010000	°1.1357	-1.62112t+06 -1.71762t+07	L.57597E+06	0. U.	ć. ć.	-1.621126+06 -1.56C026+C7 -3.12C0	1.cc
201020000 201030000 201040000	.33296 1.1871 216.21	5114.0 -2.52530E+04	-8676.9 -7349.3 C. -1.01950E+04	0.	C. C.	-2234.1 -2.504282+04 -1.019386+04	1.44
201050000 201050000 201070000 2010500000	25.45C 209.19 - 362C3	-4891.7 -2.466316+04	3489.0 C. -1.089236+04	0. 0. 0.	C. C.	-13772 -2.44539E+C4 -36203 -1.08903E+C4	1.49 1.44
203020000	105.64 27.65 66.47 66.47	-7.41091E+04 C. C.	C. C. C.	C . 0 . 0 .	C. C.	-7.405922+04 26045 66047 -1.1340	1.54
203050000 203060000 203070000	-1.6:97	-7.05485E+04	-1226.6	0. 0. 0.	· · · · · · · · · · · · · · · · · · ·	-6.94274E+C4 -1.6197 -3.69713E+C4	1.61
203090CC0 203100CC0 203110CC0	-1.5769 -2.667 -2.5355 -2.5355	с. с. с.	0. 0. 0.	0.	· · · · · · · · · · · · · · · · · · ·	-2.5255 -2.5355 -2.9839	1.54
203130CCC 203140CCO 203140CCO	-3.3721 -3.7512 -4.0570	C.	с. с. с.	0.00.00	· · · · · · · · · · · · · · · · · · ·	-3.7512 -4.0570 -4.3083	1.54
203176CC0 203186CC0 203186CC0 203190CC0	-4.5073 -4.6550 8.1956	C. C. C. - c. 95467E+04	C. -1979.7 C.	0.	C. C.	-4.6550 -1971.5 -6.82C48E+C4	1.54
203210CC0 203220CC0 203230CC0	-5.7654 -5.7656 -5.677 -5.6737	C. C.	· · · · · · · · · · · · · · · · · · ·	0.		-5.7456	1.54
203250CC0 20326CCC0 203270CC0	-5.636C 12.7C7 1666.7	C. -6.59022E+04	6.34.13 C.	0. 0.		-421.42 -6.42335E+C4 -4.3892	1.50
205010000	¢.	(.	۲.	0.	L.		



12.03.20.

FERCE-TIME HISTORY FROM RELAPS DUTPUT CATA - SUMMARY OF MAXIMUM POSITIVE SUBFORCES SAMPLE PROBLEM - RELIEF VALVE DISCHARGE W/D LCCP SEAL 10/15/82

FORCE	SHEAR FORCE	INLET INT. FORCE (NEWTONS)	CUTLET INT. FORCE (NENTONS)	FORCE (NENTCAS)	CUTLET EXT. FORCE (NEWTONS)	MAXIPUH FCRCE (NENTONS)	FORCE (SECONDS)
101 102 103 104 105 106 107 108	-109.84 -1482.88 2517.55 -201.01 -1341.65 3772.9 -22744.0 3548.9	7.41691E+64 7.05485E+04 6.95485E+04 6.95467E+04 6. 5.55622E+04 6.	C. 7.05485E+04 C. 6.95466E+04 C. 6.95466E+04 C. 6.59C22E+04		······································	7.4C592E*C4 6.9C658E*C4 7.3C641E*C4 3.65713E*C4 6.82C48E*C4 7.35195E*C4 6.36582E*C4 6.36582E*C4 6.36582E*C4 6.94511E*C4	•559 1.01 1.01 1.02 1.02 1.02 1.02
2 2 1				· · · · ·			
4							
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			and a star stary.				

FORCE-TIME HISTORY FROM RELAPS UNTFUT DATA - SUMMARY OF MAXIMUM NEGATIVE SUBFORCES SAMPLE PROBLEM - RELIEF VALVE DISCHARGE W/D LCCP SEAL

10/15/82	12.03.20.	l
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1 2 3	FOPCE	SHEAK FORCE	INLET INT. FURCE (NEWTUNS)	CUTLET INT. FORCE (NE.TUNS)	INLET EXT. FORCE (NE.TCNS)	CUTLET EXT. FURCE (NE +TCNS)	FCRCE (NEWTONS)	FORCE (SECONDS)
2 5 7 8 9 0 1 2 7	101 102 103 105 105 106 107 108	-4.13412E-03 46626 .520C6 -9.9679 18.477 -13.059 31.658	-1317.2 -1220.6 -1233.1 -1979.7 -434.13 C.	C. -1220.6 C. -1979.7 C. -434.13		c. c. c. c. c.	-1317.2 -1221.1 -1220.1 -1223.4 -1965.6 -1961.2 -447.19 -402.47	1.52
1-4 4 5 6 7 8								
9 0 · · · · · · · · · · · · · · · · · ·								
18 76 17 19 19								
32 37 51								
	•							

•	3 4		•				
FCRCE-T S&MPLE	IPE HISTORY FROM PROBLEM - RELIE	RELAPS OUTPUT DI F VALVE DISCHARG	ATA - SUMMARY CF E ¥∕O LCCP SEAL	MAXIMUM POSITI	VE CCMBINEC FORCE	S C/15/82	12.03.2C.
FORCE	SHEAR FORCE	INLET INT. FORCE (NEWTONS)	CUTLET INT. FURCE (NETTENS)	INLET EXT. FGRCE (NEWT(NS)	CUTLET EXT. FURCE (NENTENS)	FORCE (NELTONS)	FURCE SECONDS1
201 202 203	236.74 847.04 1019.7	-5192.1 -1.216366+04 -1.185676+04	9197.6 2.11611E+04 1.71427E+04	U. U.	ç:	4242.3 9864.6 6305.7	1:43
<u>г</u>							
		10.01.00					
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	r there brochard	THE REAL				TIME CE
SHEAR FORCE	INLET INT. FCKCE (NEWTGNS)	CUTLET INT. FORCE (NEWTONS)	INLET EXT. FORCE (NEWTONS)	EUTEET EXT. FURCE (NEWTONS)	FCRCE INENTONS]	FORCE
153.6C 48Cc.3 2754.6	-9424.1 -8.122928+04 -3.221658+04	3813.6 3.39981E+94 2.25594E+04	0 • 0 •	č:	-5456.8 -4.24248E+C4 -69C2.5	1.46 .248 .247
• 2184 TIME-FOR	CE RECORDS HAVE	BEEN WEITTEN TO	THE STRUCTURAL C	OTPLT FILE		
				Sec. States		
			·····			
<u> </u>	and the second secon					
	SHEAS FCRCE 153.6C 46CC.3 2754.6 • 2184 TIPE-FOR	INLET INT.	SMEAR FERCE INLET INT. FERCE CUTLET INT. FORCE 153.6C -5424.1 3013.6 2754.0 -5.221651.04 3.359016.04 2184 TIME-FORCE RECORDS HAVE BEEN NETITEN TO	SWEAS FORCE INLET INT. FURCETINT. INLET (XT. SWEAS FORCE INEWTONS) FORCETONS) INDEED (XT. 153.40 2754.0	SPEAR FORCE INLET INT. FUTCET INT. FUTCET INT. FUTCET ENT. 153.4C -542451 303366 0: C: 2754.0 -542451 0: C: 2164 TIPE-FORCE RECORDS HAVE BEEN AFITTEN TO THE STRUCTURAL COTPUT FILE	SHEAR FORCE HOLET INT. HOLET INT. HOLET INT. HOLET CASS HOLET EXT. HOLET EXT.