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Experiment Data Report For Semiscale Mod-2A Steam Line Break Experiments (Tests S-SF-4 and S-SF-5)

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**EXPERIMENT DATA REPORT FOR
SEMISCALE MOD-2A STEAM LINE BREAK
EXPERIMENTS (TESTS S-SF-4 AND S-SF-5)**

Ronald A. Larson

Published October 1982

**EG&G Idaho, Inc.
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ABSTRACT

This report presents test data recorded for Tests S-SF-4 and S-SF-5 of the Semiscale Mod-2A Primary Steam and Feedwater Line Break Experiment Series. These tests are part of a series of Semiscale tests that investigate the thermal-hydraulic phenomena resulting from operational transients involving rupture of the steam line piping on the secondary side of a pressurized water reactor. Experimental data from the tests are used to develop and assess the analytical capability of computer models used to predict the results of such a rupture in the steam line piping and evaluate the operational procedures involved in system recovery.

The primary objectives of the tests were to determine the effects of a secondary-side transient on the primary side of the system, with 100% (S-SF-4) and 50% (S-SF-5) ruptures of the main steam line piping, and to provide data for water reactor safety codes and scoping for future tests.

This report presents the uninterpreted data from Tests S-SF-4 and -5 for analysis. The data, presented as graphs in engineering units, have been analyzed only to the extent necessary to ensure that they are reasonable and consistent.

SUMMARY

Tests S-SF-4 and S-SF-5 were steam line break tests associated with the Semiscale Mod-2A Steam and Feedwater Line Break Experiment Series conducted by EG&G Idaho, Inc., for the United States Government. These tests investigated the thermal-hydraulic phenomena resulting from various size ruptures in the main steam line of a pressurized water reactor (PWR). Specifically, Tests S-SF-4 and -5 simulated a transient which resulted in overcooling of the primary side of a PWR system due to the temporarily enhanced heat sink during secondary side blowdowns.

The Semiscale Mod-2A system is equipped with a pressure vessel that contains an electrically heated core, other simulated reactor internals, and an external downcomer assembly; an intact loop with steam generator, pump, and pressurizer; and a broken loop with steam generator, and pump.

The main steam line break tests were initiated from hot standby conditions, which results in the

greatest cooldown prediction. The break nozzle sizes were scaled to represent 100% (S-SF-4) and 50% (S-SF-5) of the area of a Westinghouse four-loop PWR. These tests duplicated, as nearly as possible, the conditions of a typical PWR system. In addition, a long-term recovery procedure was attempted using a primary feed and bleed during the tests.

Generally, Tests S-SF-4 and -5 proceeded as specified. Conditions that did not conform to the specified test configuration were considered acceptable for analysis within the test objectives.

This report presents the digital data from Tests S-SF-4 and -5 with brief comment. The data are presented in the form of graphs in engineering units, and are also available from the NRC/DAE Data Bank at the Idaho National Engineering Laboratory. Address inquiries to NRC/DAE Data Bank Administrator, EG&G Idaho, Inc., P.O. Box 1625, Idaho Falls, Idaho 83415.

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- 241. Liquid level in broken loop steam generator secondary side downcomer, Test S-SF-4 (LBS + 825 + 50)
- 242. Liquid level in broken loop steam generator secondary side riser, Test S-SF-4 (LBS + 463 + 89)
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- 244. Liquid level in pressurizer, Test S-SF-4 (LPRZ146 + 25)
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366. Fluid temperature in intact loop steam generator, secondary side, Test S-SF-5
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368. Fluid temperature in intact loop steam generator, secondary side, Test S-SF-5
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369. Fluid temperature in intact loop steam generator, secondary side, Test S-SF-5
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370. Fluid temperature in intact loop steam generator, secondary side, Test S-SF-5
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371. Fluid temperature in intact loop steam generator, secondary side, Test S-SF-5
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372. Fluid temperature in intact loop steam generator, secondary side, Test S-SF-5
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381. Fluid temperature in broken loop steam generator, secondary side downcomer, Test S-SF-5 (TFBS*D + 457)
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385. Fluid temperature in broken loop steam generator, secondary side, Test S-SF-5 (TFBS + LC84)
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- 391. Fluid temperature in broken loop steam generator, secondary side,
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- 392. Fluid temperature in broken loop steam generator, secondary side,
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- 393. Fluid temperature in broken loop steam generator, secondary side,
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- 394. Fluid temperature in broken loop steam generator, secondary side,
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- 395. Fluid temperature in broken loop steam generator, secondary side,
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- 396. Fluid temperature in broken loop steam generator, secondary side,
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- 397. Fluid temperature in broken loop steam generator, secondary side,
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- 398. Fluid temperature in broken loop steam generator, secondary side,
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- 452. Core heater temperature, Rod B-4, Test S-SF-5 (THV*B4 + 140)
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- 454. Core heater temperature, Rod C-3, Test S-SF-5 (THV*C3 + 140)
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- 456. Core heater temperature, Rod C-4, Test S-SF-5 (THV*C4 + 187)
- 457. Core heater temperature, Rod D-2, Test S-SF-5 (THV*D2 + 16)
- 458. Core heater temperature, Rod D-2, Test S-SF-5 (THV*D2 + 254)
- 459. Core heater temperature, Rod D-2, Test S-SF-5 (THV*D2 + 321)
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- 470. Core heater temperature, Rod C-1, Test S-SF-5 (THV*C1 + 79)
- 471. Core heater temperature, Rod C-1, Test S-SF-5 (THV*C1 + 211)
- 472. Core heater temperature, Rod C-1, Test S-SF-5 (THV*C1 + 292)
- 473. Core heater temperature, Rod C-5, Test S-SF-5 (THV*C5 + 133)

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EXPERIMENT DATA REPORT FOR SEMISCALE MOD-2A MAIN STEAM LINE BREAK EXPERIMENTS (Tests S-SF-4 and S-SF-5)

INTRODUCTION

The Semiscale Mod-2A experiments represent the current phase of the Semiscale Program conducted by EG&G Idaho, Inc., for the United States Government. The program, sponsored by the Nuclear Regulatory Commission (NRC) through the Department of Energy, is part of the overall NRC Water Reactor Research Program to investigate the response of a pressurized water reactor (PWR) system to hypothesized loss-of-coolant accidents (LOCAs) or abnormal operating transients. The underlying objectives of the Semiscale Program are to quantify the physical processes that control system behavior and to provide an experimental data base for assessing reactor safety evaluation models. The program has the further objective of providing support to other experimental programs in the forms of instrument assessment, test series optimization, selection of test parameters, and comparative evaluation of test results.

The Steam and Feedwater Line Break Scoping Experiment Series (Series SF) was formulated in response to NRC needs concerning specific licensing issues centered around PWR transient response during steam generator secondary side main steam line or main feedwater line ruptures.

Tests S-SF-4 and S-SF-5 were conducted in the Semiscale Mod-2A facility on May 26, 1982 and June 3, 1982, respectively, as part of the main steam line break in the SF test series. The steam line break tests investigate the thermal and hydraulic phenomena that occur when overcooling of the primary side takes place due to the temporarily enhanced heat sink caused by a secondary side blowdown. The tests were initiated from hot standby conditions because it was predicted to be a more limiting case for excessive primary side cooldown. The primary objectives of Tests S-SF-4 and -5 were fourfold; to determine the primary-to-secondary heat transfer characteristics as a function of time and steam generator inventory; to provide a reference data

base for assessing the capabilities of water reactor safety codes to predict integral system behavior in response to secondary side transients; to provide a data base for specifying future experiments; and to characterize the influence of boundary conditions such as break size, loss of offsite power assumptions for Test S-SF-5, and emergency core cooling and feedwater train performance.

The break sizes for Tests S-SF-4 and -5 were scaled from a Westinghouse four-loop plant. The break nozzle was sized to provide the scaled critical flow rate reported for the main steam line flow restrictors at normal operating pressure. The scaling basis for Tests S-SF-4 and -5 were 100% and 50%, respectively, of the 16-in.-inner-diameter main steam line flow restrictor. Due to the "scoping" nature of these experiments, it is realized that they will not simulate the exact response of a Westinghouse plant to these transients. However, these experiments will identify the dominant parameter trends which ultimately control the severity of the transient.

This report presents the data from Tests S-SF-4 and -5 in an uninterpreted, but readily useable form, for use by the nuclear community in advance of detailed analysis and interpretation. A brief description of the system configuration, procedures, and sequence of events for Tests S-SF-4 and -5 is presented, followed by the data graphs, comments, and supporting information necessary for interpretation of the data. An overall description of the Semiscale Program and test series, with a more detailed description of the Steam and Feedwater Line Break Series are contained in References 1 and 2. Preliminary analysis and interpretation of the data are presented in Reference 3.

Information on the data acquisition system, posttest adjustments made to the data, and the methodology used to establish measurement uncertainty limits are presented and explained in Reference 4.

SYSTEM PROCEDURES, CONDITIONS, AND EVENTS FOR TESTS S-SF-4 AND S-SF-5

System Configuration

The Semiscale Mod-2A primary system was scaled using a four-loop Westinghouse design as the reference. The system used for these tests consists of a core vessel with simulated reactor internals, including an electrically powered 25-rod core and an external downcome; an intact loop with steam generator and reactor coolant pump (RCP), with pressurizer connected, through an orificed surge line, to the hot leg of the intact loop, at Spool Piece 3; and a broken loop with steam generator and RCP, as shown in Figures 1 and 2. Figure 3 shows a cross section of the core vessel and external downcomer. The vessel core consists of a 5 x 5 array of internally heated electric rods, 23 of which were powered (Rods A1 and E-5 were unpowered). The rods are geometrically similar to nuclear fuel rods, with a heated length of 3.66 m and an outside diameter of 1.072 cm. The core power was set up to provide a symmetric chopped cosine axial power distribution with a peak-to-average power ratio of 1.25 between the low and high power bus to provide a total core power of 30 kW, plus heat loss. (The high power bus consisted of the 9 center rods; the low power bus consisted of the 14 peripheral rods.) Figures 4 and 5 show the instrumentation penetrations of the core vessel and downcomer, respectively. A plan view of the core and the locations of the heater rod thermocouples are shown in Figure 6. Table 1 presents a comparison of the elevation differences between the major components.

The intact and broken loop steam generators are of the same two-pass, tube-and-shell design. Primary fluid flows through vertical, inverted-U-shaped tubes, and secondary coolant passes from bottom to top through the shell side. The intact loop steam generator has two short, two medium, and two long tubes representative of the range of bend elevations in PWR steam generators. The broken loop steam generator utilizes only one long and one short tube. An "off-center" arrangement of the tubes was required to provide better volume scaling of the secondary. The same tube stock (2.22-cm OD x 0.124-cm wall) and tube spacing (3.175-cm triangular pitch) used for PWR U-tubes were used in the Semiscale steam generators. Since the heat

transfer area was specified by the ratio of PWR-to-Semiscale core power, the number of tubes was thereby fixed by the specified tube diameter and lengths. Fillers were installed in the shell side to provide a more properly scaled secondary fluid volume. Elevations of the Semiscale Mod-2A steam generator nozzles, plenums, and tubes are similar to those of a PWR; however, the steam dome is shorter than that of a PWR, and the steam drying equipment is of a simpler and less efficient design.

The steam generator primary and secondary sides are extensively instrumented, as shown in Figures 7 and 8 for the intact and broken loop, respectively. At several axial locations, pairs of primary and secondary fluid thermocouples, along with primary tube wall metal thermocouples have been attached to the tube walls. One long and one short tube in each steam generator are instrumented; the middle tubes of the intact loop steam generator have no thermocouples installed. In addition to the tube thermocouples, the steam domes have fluid thermocouples, and the downcomers have fluid thermocouples at several axial locations. Other steam generator instrumentation includes primary tube (primary side) and secondary (shell side) differential pressure ports at several elevations, allowing measurement of collapsed liquid levels in the inlet side of the primary tubes and in the secondary downcomer and riser.

Separate auxiliary feedwater pumps were lined up to discharge into the upper feed ring of each steam generator. Flow and temperature measurements are provided.

The steam line break simulation assembly was connected to the intact and broken loop steam generators as shown in Figure 9. The break effluent from the intact loop steam generator was routed to the pressure suppression header, and the break effluent from the broken loop steam generator was routed through the condensing coils into the catch tanks. The condensing system is shown in Figure 10.

Safety injection pumps were lined up to discharge only into the cold leg of the intact loop, at Spool Piece 22. Flow and temperature measurements were provided.

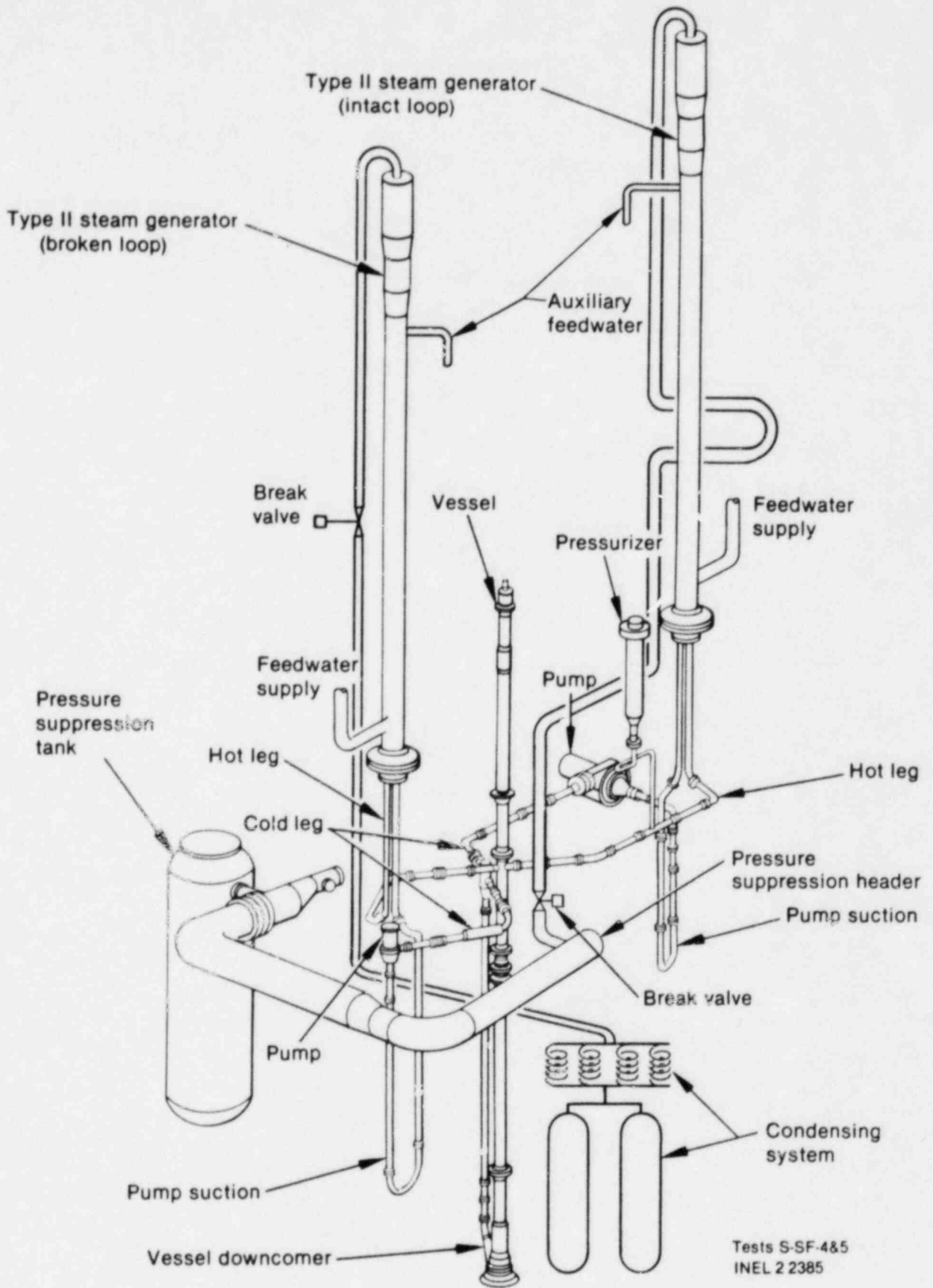


Figure 1. Semiscale Mod-2A system configuration for main steam line break test—*isometric*.

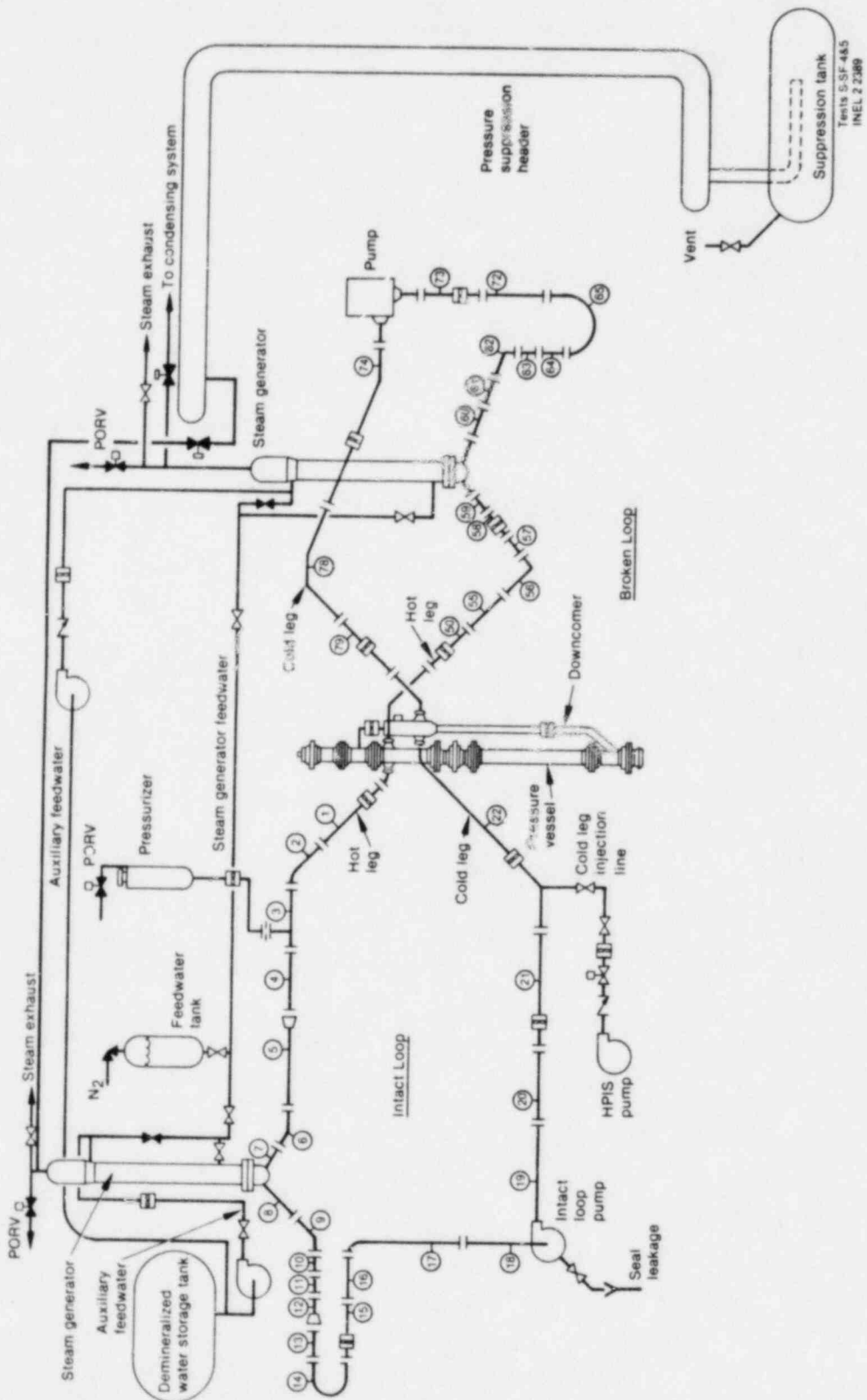


Figure 2. Semicale Mod-2A system configuration for main steam line break test—schematic.

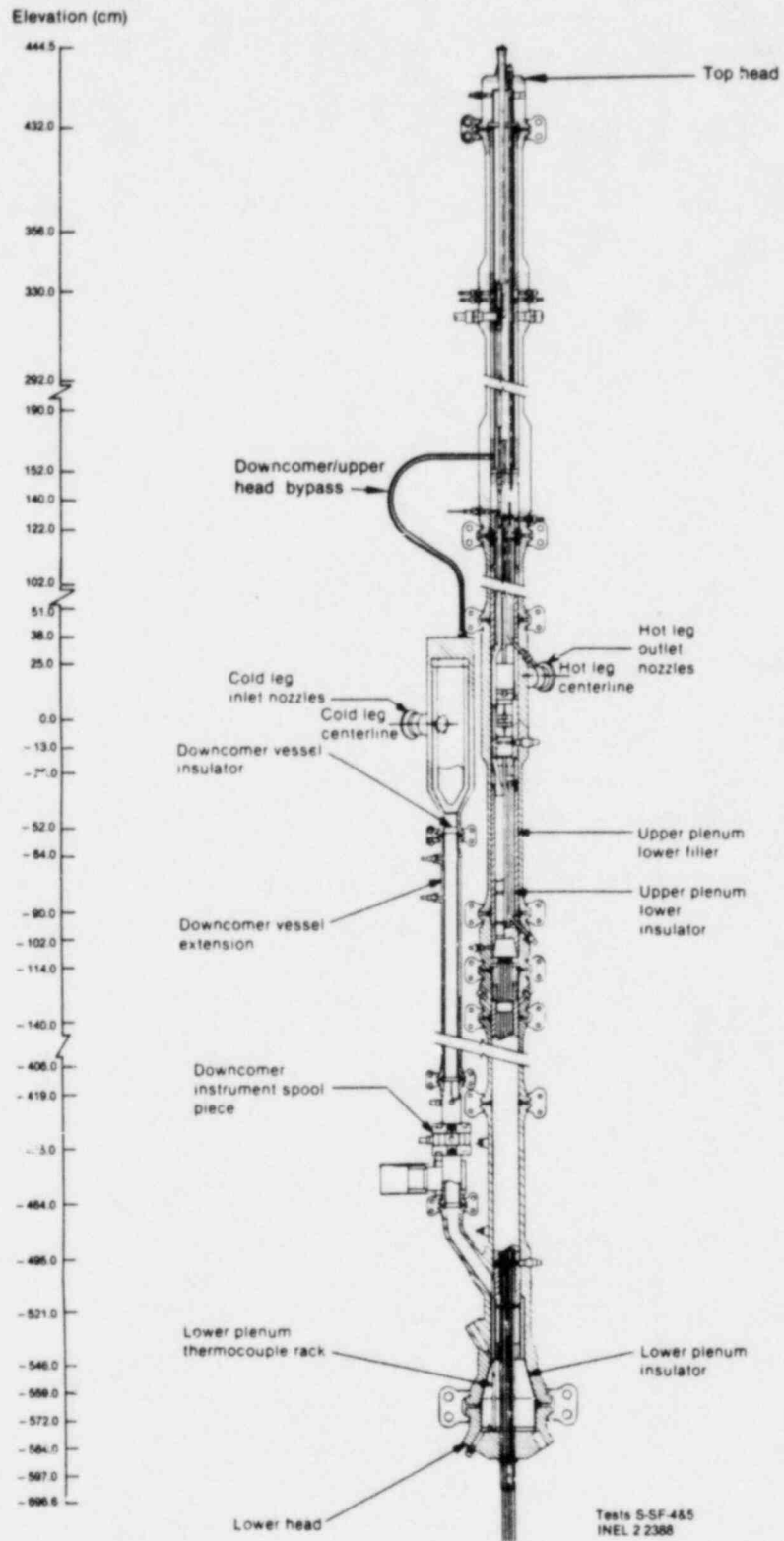
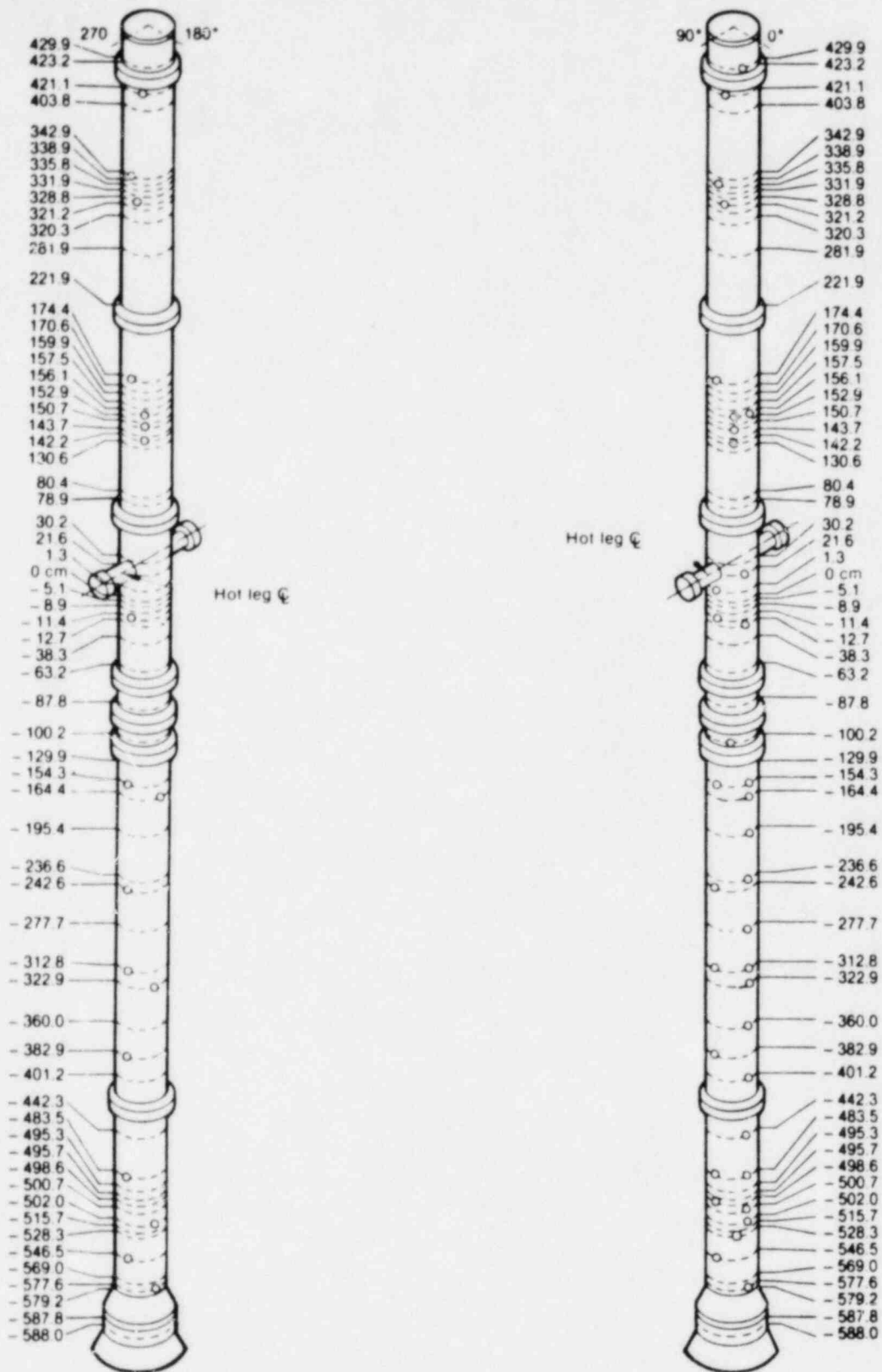


Figure 3. Semiscale Mod-2A pressure vessel and downcomer—cross section.



Tests S-SF-4&5
INEL 2 2384

Figure 4. Semiscale Mod-2A pressure vessel— isometric showing penetrations.

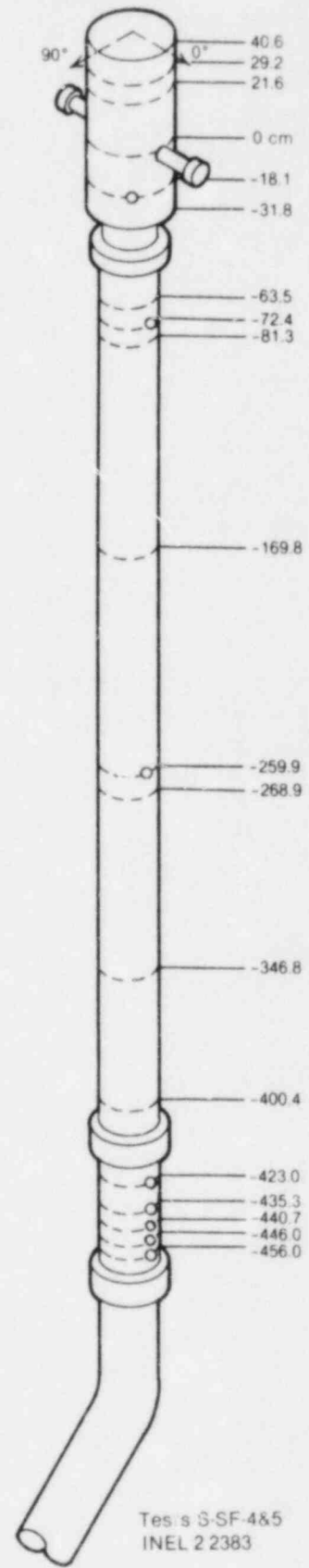
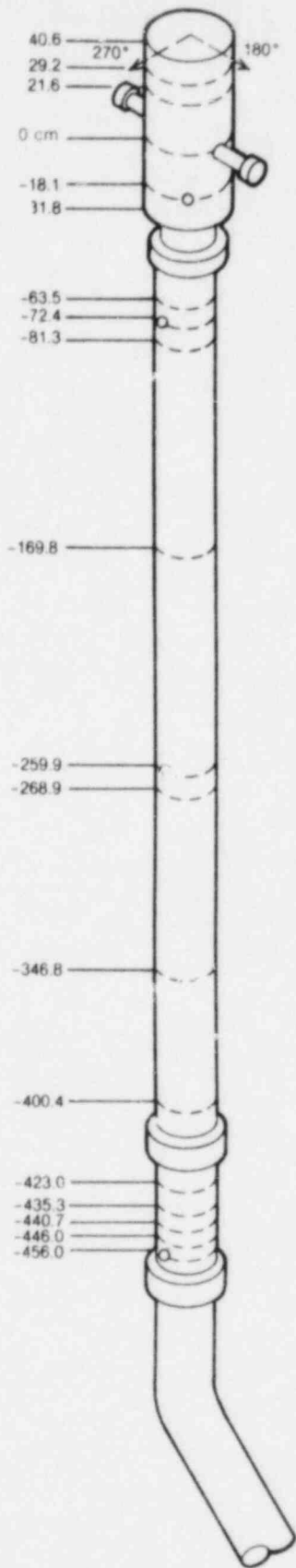
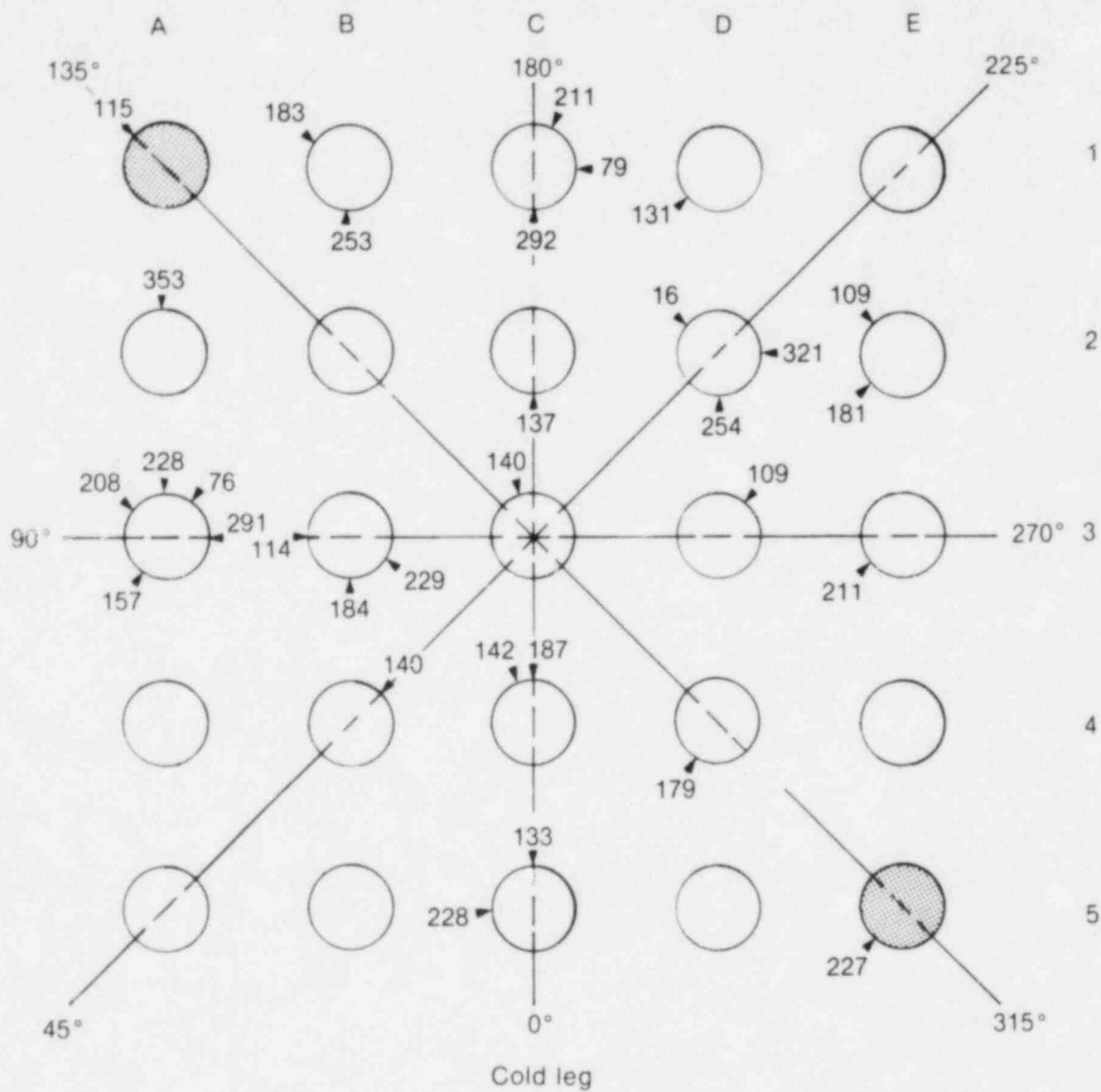


Figure 5. Semiscale Mod-2A downcomer—isometric showing penetrations.



Tests S-SF-4&5
INEL 2 2380

Figure 6. Semiscale Mod-2A heated core plan view.

Table 1. Semiscale Mod-2A system reference elevations^a

	Centerline		Pressurizer Exit	Top of Tube Sheet ^b		Bottom of Core Heated Length
	Cold Leg	Hot Leg		I.S.G.	B.S.G.	
Cold leg centerlines	0	-20	-150	-260	-260	+496
Hot leg centerlines	+20	0	-130	-240	-240	+516
Pressurizer exit flange face	+150	+130	0	-130	-130	+646
I.S.G. top of tube sheet	+260	+240	+130	0		+756
B.S.G. top of tube sheet	+260	+240	+130	0	0	+756
Bottom of core heated length	-496	-516	-646	-756	-756	0

a. All dimensions in centimeters.

b. I.S.G. = intact loop steam generator; B.S.G. = broken loop steam generator.

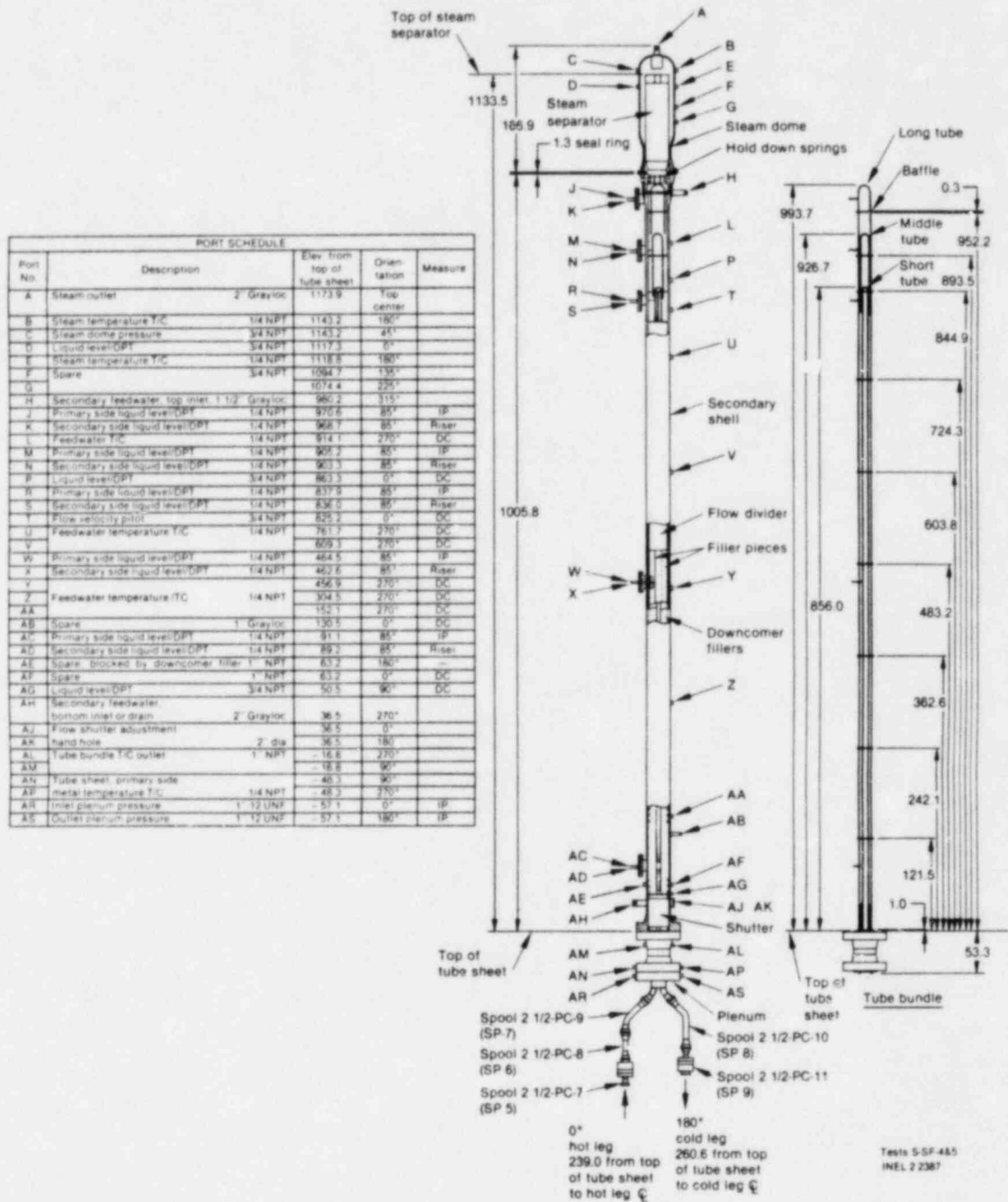


Figure 7. Semiscale Mod-3A intact loop steam generator instrumentation.

PORT SCHEDULE					
Port No.	Description		Elev. from top of tube sheet	Orientation	Measure
A	Steam outlet	2" Grayloc	1173.9	Top center	
B	Steam temperature T/C	1/4 NPT	1143.2	180°	
C	Steam dome pressure	3/4 NPT	1143.2	45°	
D	Liquid level DPT	3/4 NPT	1117.3	0°	
E	Steam temperature T/C	1/4 NPT	1118.8	180°	
F	Spare	3/4 NPT	1094.7	135°	
G			1074.4	225°	
H	Secondary feedwater top inlet 1 1/2" Grayloc		960.2	135°	
J	Primary side liquid level DPT	1/4 NPT	970.6	85°	IP
K	Secondary side liquid level DPT	1/4 NPT	968.7	85°	Riser
L	Feedwater T/C	1/4 NPT	914.1	270°	DC
M	Liquid level DPT	3/4 NPT	914.1	90°	DC
N	Liquid level DPT Blocked by downcomer filter	3/4 NPT	863.3	0°	
P	Liquid level DPT	3/4 NPT	863.3	270°	DC
R	Primary side liquid level DPT	1/4 NPT	837.9	85°	IP
S	Secondary side liquid level DPT	1/4 NPT	836.0	85°	Riser
Y	Flow velocity pilot	3/4 NPT	825.2	270°	DC
U	Flow velocity pilot Blocked by downcomer filter	3/4 NPT	825.2	0°	
V	Feedwater temperature T/C	1/4 NPT	761.7	270°	DC
W			606.3	270°	DC
X	Primary side liquid level DPT	1/4 NPT	464.5	85°	IP
Y	Secondary side liquid level DPT	1/4 NPT	462.6	85°	Riser
Z	Feedwater temperature T/C	1/4 NPT	456.9	270°	DC
AA			324.5	270°	DC
AB			152.1	270°	DC
AC	Spare Blocked by downcomer filter	1" Grayloc	130.5	0°	
AD	Primary side liquid level DPT	1/4 NPT	81.1	85°	IP
AE	Secondary side liquid level DPT	1/4 NPT	80.2	85°	Riser
AF	Spare blocked by downcomer filter 1" NPT		63.2	180°	
AG			63.2	180°	
AH	Spare	1" NPT	63.2	270°	DC
AJ	Liquid level DPT	3/4 NPT	50.5	90°	DC
AK	Secondary feedwater bottom inlet or drain	2" Grayloc	36.5	270°	
AL	Flow shutter adjustment hand hole	2" dia	36.5	180°	
AN	Tube bundle T/C outlet	1" NPT	-16.8	270°	
AR	Tube sheet primary side metal temperature T/C		-46.3	90°	
AS	Inlet plenum pressure	1" 1/2 UNF	-57.1	180°	
AU	Outlet plenum pressure	1" 1/2 UNF	-57.1	0°	

Notes:
All dimensions are cm reference (1 inch = 2.54 cm)

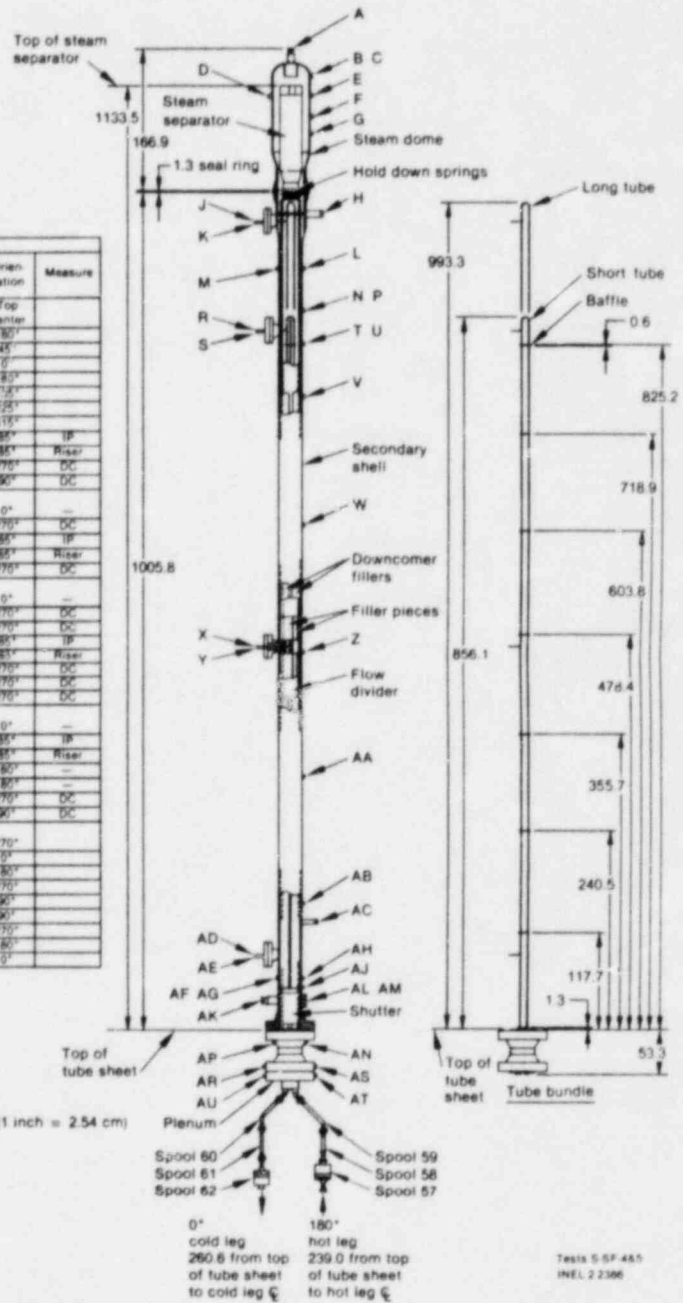


Figure 8. Semiscale Mod-2A broken loop steam generator instrumentation.

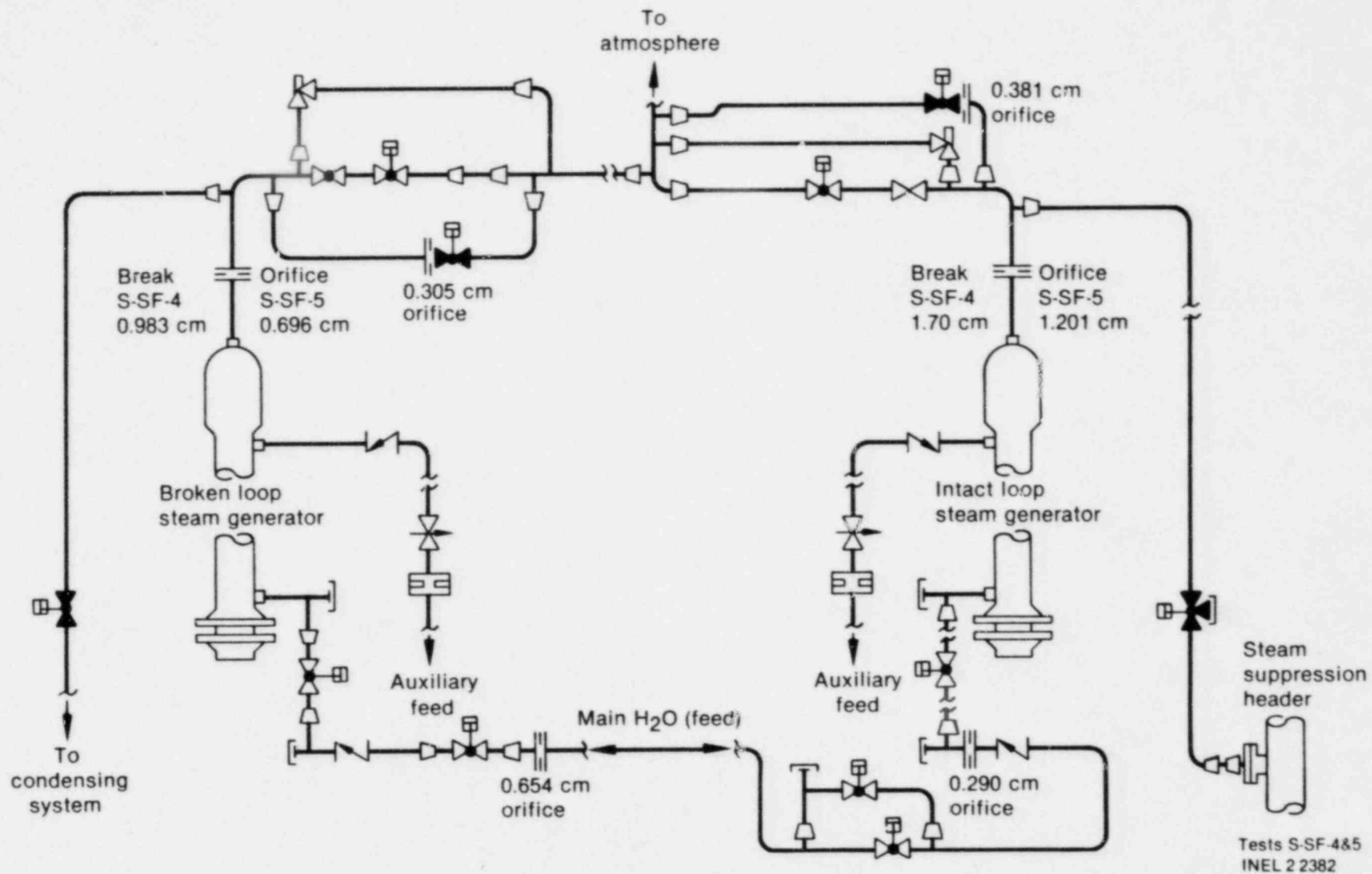


Figure 9. Semiscale Mod-2A break piping for main steam line break Tests S-SF-4 and -5.

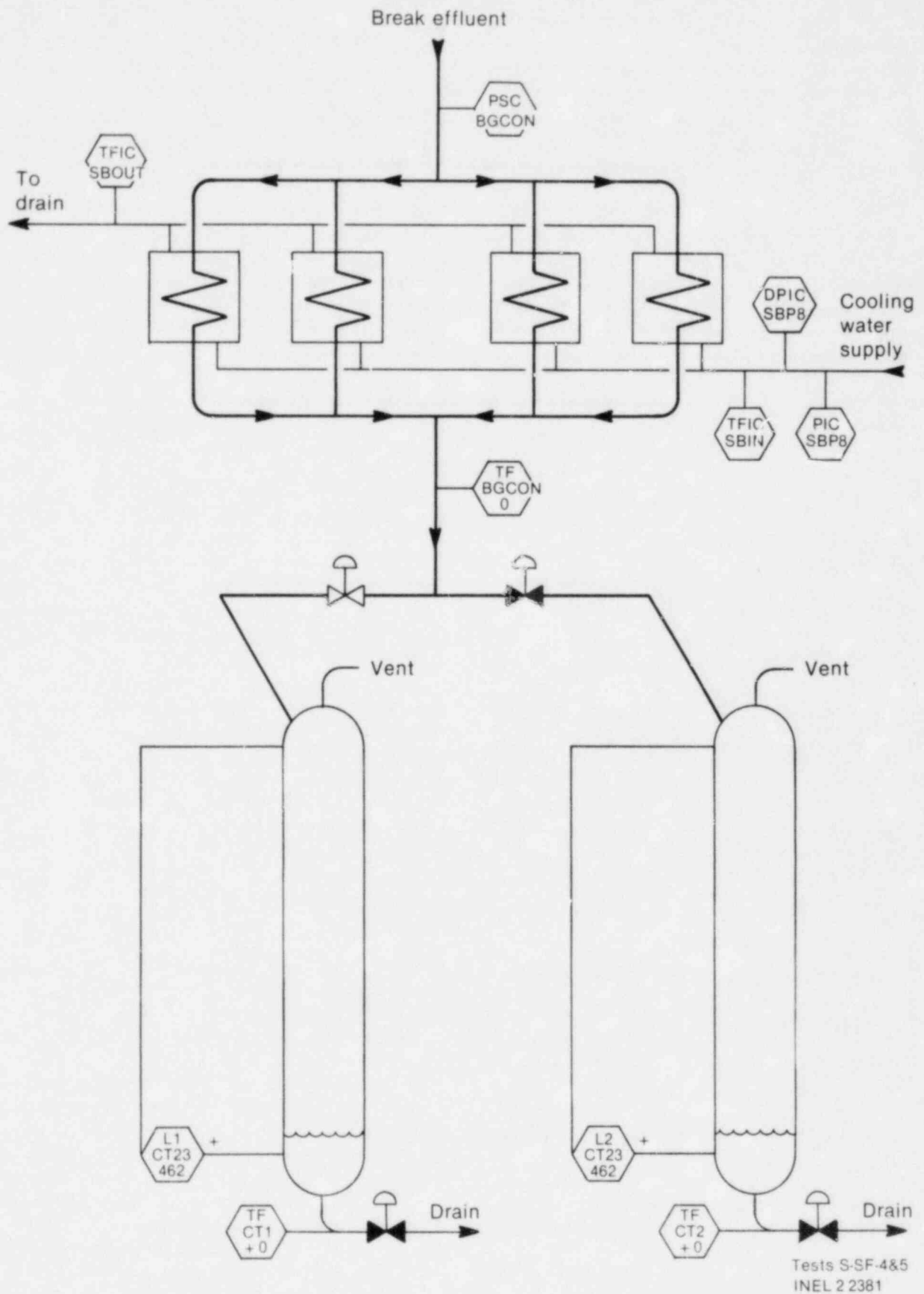


Figure 10. Semiscale Mod-2A break effluent measurement system (condensate system) for Tests S-SF-4 and -5.

External band heaters on the loop piping, downcomer, and core vessel were powered continuously to maintain an adiabatic primary pressure boundary.

Test Preparation

In preparation for each of the two tests, the primary system was filled with treated demineralized water and vented at all high points to ensure a liquid solid condition. A leak check was performed and all measurement transducers were vented and their conditioners/amplifiers were balanced and zeroed. The feedwater supply tank was filled and heated, and initial levels were established in the steam generator secondaries. All auxiliary system valve liquids were set and verified, as were all process alarm, trip, and control functions.

Warmup

Warmup of the primary system to initial test conditions was accomplished using the core heaters, pressurizer heaters, external band heaters, and RCPs, in a sequence that closely resembled a full-scale PWR system, but that is much shorter due to the electric core. The purification and sampling systems were valved-in during warmup to maintain water chemistry and to obtain primary coolant samples at initial conditions for subsequent analysis. At 50-K intervals, detector readings were sampled to check measurement transducer integrity and data acquisition system performance. Also, other checks were performed at various times during warmup to verify total system operational integrity.

Test Sequence

Initial conditions for the two tests were specified to conform to typical PWR operating values for hot standby conditions. Table 2 presents the specified values versus the actual measured values for selected parameters at the start of each test.

Once initial conditions were achieved, they were held long enough to assure reasonably steady state operation of the reactor coolant system (RCS).

The data acquisition system was then started on a continuous data scan to record the initial test values and to verify the steady state condition; it then remained on throughout the tests, with time zero designated as the instant the quick-opening break valve was energized to start the main steam line rupture simulation.

Two seconds prior to rupture initiation (-2 s), the closed-loop purification system was isolated from the RCS, and the pressurizer level-controlled charging pumps were disabled. Also at this time, feedwater valve closure was initiated on both steam generators, so that the valves would be shut by zero seconds.

The operation of active components in the system during the transient was by prespecified control curves (except for core power control) that simulate the operation expected to occur during a transient in a PWR plant. Control curves are specified in Reference 2.

The core power for Test S-SF-4 was computer controlled to perform on-line calculations and adjust the power in response to measured conditions. The controller samples information during a transient from internal rod cladding thermocouples, in-core fluid thermocouples, and the core power supply. For each time increment, the equivalent power was calculated for a nuclear core subjected to the same thermal-hydraulic conditions and the Semiscale core power was adjusted accordingly. For Test S-SF-5, the core power was set at 30 kW, plus allowing for heat loss, and was manually controlled throughout the test so as to provide a more severe cooldown than that which occurred during Test S-SF-4.

The main coolant pumps maintained their initial speed until 594 s after transient initiation for Test S-SF-4 and 404 s for Test S-SF-5, at which time the broken loop pump began a 60-s decay and the intact loop pump began a 120-s decay.

The safety injection (SI) pump flow rate was controlled to simulate the injection systems of a PWR plant. For both tests, the SI began by following a high head injection curve and then switching to a low head SI curve. For Tests S-SF-4 and -5, the high head SI started at 32 and 74 s and terminated at 510 and 404 s, respectively. The low head SI was manually started at 3487 and 1715 s,

Table 2. Specified versus actual initial conditions for Tests S-SF-4 and S-SF-5

Parameter	Specified Value	Actual Values ^a	
		S-SF-4	S-SF-5
Pressurizer pressure (MPa) P*PPZ + 158	15.5 ± 2	15.5	15.6
Pressurizer liquid mass (kg) LPRZ146 + 25	10.4 ± 0.2	— ^b	— ^b
Total core power (kW) ^c KWH*TOTC	30	97	108
Cold leg fluid temperature (K) TF1*22/TFB*79	557/557	555/556	557/555
Cold leg volumetric flows (L/s) Q1*21/QB*79	— ^d /— ^d	9.4/3.1	9.4/3.2
Steam Generator			
Secondary pressure (MPa) ^e PIS*1117/PBS*1117	5.85/5.85	6.8/6.8	6.8/6.4
Collapsed liquid level (cm) ^e LIS1117 + 50 S-SF-4/S-SF-5 LBS1117 + 50 S-SF-4/S-SF-5	1020/950 1020/500	1067 933	969 480
Feedwater temperature (K) TFSC*IGFWL/TFSC*BGFWL	495/495	556/556	503/553

a. As recorded and averaged from -20 to -3 s by the DDAPS.

b. DDAPS pressurizer level measurement was erroneous. Process measurement indicated the specified level.

c. Core power was adjusted to compensate for environmental heat loss.

d. A 3:1 ratio was specified. Actual values depend only on achieving the specified core differential temperature.

e. Secondary side conditions were adjusted to obtain required primary side temperature.

respectively, and continued to the end of the tests. For S-SF-4 the high head SI was set to actuate by a low pressure signal of 14.4 MPa from the pressurizer. Test S-SF-5 had a programmed 25-s delay after 14.4 MPa before SI actually commenced.

Auxiliary feedwater to both the intact and broken loop steam generators was set to be initiated when the pressure in the broken loop steam generator steam dome reached 4.13 MPa, and the feed continued until 516 s for Test S-SF-4 and 404 s for Test S-SF-5, at which times the

steam generator auxiliary flow was terminated. The operational events for both tests are listed in Tables 3 and 4.

For each test, the basic recovery mode was to establish and maintain adequate core cooling by RCS feed and bleed using the SI system and the pressurizer power-operated relief valve (PORV). This is an alternate method of decay heat removal, which is useful in accidents in which the steam generator secondaries are not available as heat sinks.

Table 3. Sequence of events, Test S-SF-4

Plot Time (s)	Event
-30	Data acquisition system began recording test data
-2	Closed-loop purification system isolated; automatic charging pumps, pressurizer heaters, and intact and broken loop steam generator feed valves disabled.
0	Broken loop steam valve closed; intact loop steam valve opened; intact and broken loop main steam line break valve opened—start of transient
+32	High head safety injection started
+68	Auxiliary feedwater started to both steam generators
+483	PORV reset to 14.48 and 14.34 MPa ^a
+510	High head safety injection terminated
+516	Auxiliary feedwater terminated
+560	Core power switched to manual
+578	Drain of steam generators started
+594	120-s intact loop and 60-s broken loop pump coastdown started
+1000	Core power increased to 100 kW
+1402	Core power increased to 150 kW
+1946	PORV reset to 13.79 and 13.65 MPa
+1989	Core power decreased to 100 kW
+2611	PORV reset to 11.03 and 10.89 MPa
+2689	Core power decreased to 90 kW
+2778	Core power decreased to 80 kW
+3459	Core power decreased to 70 kW
+3487	Low head safety injection started
+3504	Core power decreased to 60 kW
+3613	Core power decreased to 50 kW

Table 3. (continued)

Plot Time (s)	Event
+ 3678	PORV reset to 9.65 and 9.51 MPa
+ 3804	PORV reset to 8.27 and 8.14 MPa
+ 3875	Core power decreased to 40 kW
+ 4534	Test S-SF-4 terminated

a. At the start of test, PORV was set to open at 16.2 MPa and close at 16.03 MPa.

Table 4. Sequence of events, Test S-SF-5

Plot Time (s)	Event
-30	Data acquisition system began recording test data
-2	Closed-loop purification system isolated; automatic charging pumps, pressurizer heaters, intact and broken loop steam generator feed valves disabled
0	Broken loop steam valve closed; intact loop steam valve opened; intact and broken loop main steam line break valve opened—start of transient
+ 74	High head safety injection started
+ 85	Auxiliary feedwater started to both steam generators
+ 240	PORV reset to 15.09 and 13.79 MPa ^a
+ 404	High head safety injection terminated; auxiliary feedwater terminated; drain of steam generators started; 120-s intact loop pump and 60-s broken loop pump coastdown started
+ 1705	PORV reset to 8.96 and 8.89 MPa.
+ 1715	Low head safety injection started
+ 1920	Leak in intact loop between Spool Pieces 21 and 22 developed
+ 2510	Test S-SF-5 terminated

a. At the start of test, PORV was set to open at 16.2 MPa and close at 16.03 MPa.

DATA PRESENTATION

This section discusses the digital data^a from Semiscale Mod-2A Main Steam Line Break Tests S-SF-4 and S-SF-5, which are presented as graphs in engineering units. Processing analysis serves only to obtain the proper engineering units and to ensure that the data are reasonable and consistent. In all cases, a homogeneous fluid was assumed when converting the transducer output to engineering units. The scales selected for the data graphs do not reflect the obtainable resolution of the measurements.

The performance of the Mod-2A system during Tests S-SF-4 and -5 was monitored by 308 and 309 measurement detectors, respectively. Of these, approximately 20 per test are not presented in this report because they were either installed on auxiliary systems that were not used, used solely for in-house processing and control, or had failed before or during the test.

The output of each detector/transducer passes through a signal conditioner and amplifier where the signal is converted to a dc voltage compatible with the Digital Data Acquisition and Processing System (DDAPS). The DDAPS accepts the voltage inputs through analog-to-digital converters and, using previously entered coefficients, converts the input to appropriate engineering units. These data are then recorded on magnetic disks, at intervals dependent on the scan rate.

Dual scan rates were used to sample the detector outputs during both tests. During the first 570 s of DDAPS operation, each channel was scanned once every 0.05 s, yielding an effective sample rate of 20 samples per second per channel. The sample rates were then reduced to accommodate the expected duration of the individual tests, and the scan was slowed to 0.55 s per channel, for an effective sample rate of 1.82 samples per second per channel.

Posttest data review and qualification were conducted by a Data Integrity Review Committee. Erroneous and superfluous measurements were

identified and deleted, and the necessary adjustments and calculations were performed on the remaining measurements. Ambiguous measurements, where the exact engineering unit value could not be verified, were retained because they can provide important information on parameter trends and timing functions. These measurements are labeled "trend information only" on the data graphs, rather than assigning a value to the uncertainty range of the measurement.

Immediately prior to each test, numerous calibration checks are performed and the data recorded. This information is used, after the fact, to adjust specific test data to offset such effects as pressure sensitivity, amplifier zero offset, and core power sensitivity.

The necessary posttest calculations include converting the voltage outputs of the densitometers to actual density (kg/m^3). This is done by setting the measured low voltage output during a subcooled condition equal to the known density at that time, and by setting the measured high voltage output during a vapor condition to the known density at that time. The density at all other times is then computed using an inverse ratio of voltage to density with the two known points used to define the values. The nonlinearity of this method across a phase change is recognized and incorporated into the derivation of the measurement uncertainty value.

In much the same manner, the valve position transducer outputs are converted from voltage to percent open, this being a direct, linear relationship.

The power "measurements" for the core and the external band heaters are not actual measurements, but are calculated from the measured voltage and current output of the individual power supplies.

The above noted adjustments and calculations were the only ones performed on the data presented herein. References 1 and 4 further describe the Semiscale data processing techniques; Reference 4 also explains the capabilities of the DDAPS and presents an analysis of the uncertainties associated with measurement data from the Mod-2A system. Figures 1 through 10 provide

a. The digital data are available from the NRC/Division of Accident Evaluation (DAE) Data Bank at the Idaho National Engineering Laboratory. Address data inquiries to NRC/DAE Data Bank Administrator, EG&G Idaho, Inc., P.O. Box 1625, Idaho Falls, Idaho, 83415.

measurement geometry information needed for interpretation of the data. Table 5 groups the measurements according to type or location, identifies the location and range of the detector, gives the actual recording range of the DDAPS, provides brief comments on the data, and

references the detector and comments to their corresponding figure. Figures 11 through 592 (data graphs) present all the data obtained, including the noted calculated parameters. These data graphs are presented on microfiche sheets, attached to the inside back cover of this report.

Table 5. Data presentation for Semiscale Mod-2A Tests S-SF-4 and S-SF-5

Measurement	Location and Comments ^a	Data Acquisition Range ^a		Figure ^a	Measurement Comments ^b
		Detector	System		
FLUID TEMPERATURE					
<i>Intact Loop</i>					
TF1*1	Hot leg, Spool 1, 50 cm from vessel center.	0 to 1533 K	0 to 820 K	11, 304	
TF1*5	Hot leg, Spool 5, 363 cm from vessel center.			12, 305	
TF1*9	Cold leg, Spool 9, 1017 cm from downcomer center.			13, 306	
TF1*17	Cold leg, Spool 17, 338 cm from downcomer center.			14, 307	
TF1*21	Cold leg, Spool 21, 138 cm from downcomer center.			15, 308	
TF1*22	Cold leg, Spool 22, 48 cm from downcomer center.			16, 309	
<i>Broken Loop</i>					
TFB*50	Hot leg, Spool 50, 73 cm from vessel center.			17, 310	
TFB*57	Hot leg, Spool 57, 278 cm from vessel center.			18, 311	
TFB*62	Cold leg, Spool 62, 962 cm from downcomer center.			19, 312	
TFB*64	Cold leg, Spool 64, 638 cm from downcomer center.			20, 313	
TFB*73	Cold leg, Spool 73, 337 cm from downcomer center.			21, 314	
TFB*76	Cold leg, Spool 76, 220 cm from downcomer center.			22, 315	
TFB*79	Cold leg, Spool 79, 78 cm from downcomer center.			23, 316	
<i>Vessel</i>					
<i>Vessel Downcomer</i>					
TFV*DC-84	Downcomer extension, 84 cm below cold leg centerline.	0 to 1533 K	0 to 820 K	24, 317	
TFV*DC-436	Downcomer extension, 436 cm below cold leg centerline.			25, 318	
<i>Vessel Lower Plenum</i>					
<i>Vessel Upper Plenum</i>					
TFV*UP-15	In vessel upper plenum, 15 cm below cold leg centerline at 180°.	0 to 1533 K	0 to 820 K	26, 319	
TFV*UP-79	In vessel upper plenum, 79 cm above cold leg centerline.	0 to 1533 K	0 to 820 K	27, 320	
<i>Vessel Upper Head</i>					
TFV*UH-180	In vessel upper head, 180 cm above cold leg centerline at 180°.	0 to 1533 K	0 to 820 K	28, 321	
TFV*UH-343	In vessel upper head, 343 cm above cold leg centerline.			29, 322	
TFV*UH-402	In vessel upper head, 402 cm above cold leg centerline.			30, 323	
TFV*UPASS	In bypass line connecting upper plenum to downcomer.			31, 324	
<i>Core Grid Spacers</i>					
<i>Grid Spacer 3</i>					
TFV*G3-46	Thermocouple in space defined by Columns B and C, Rows 3 and 4, 450 cm below cold leg centerline, 26 cm above bottom of heated length.	0 to 1533 K	0 to 1580 K	32, 325	

Table 5. (continued)

Measurement	Location and Comments ^a	Data Acquisition Range ^a		Figure ^a	Measurement Comments ^b
		Detector	System		
FLUID TEMPERATURE (continued)					
<u>Core Grid Spacers</u> (continued)					
<u>Grid Spacer 4</u>	370 cm below cold leg centerline, 126 cm above bottom of heated length.				
TFV*DL*124	Thermocouple in space defined by Columns D and E, Rows 1 and 2.			33, 326	
TFV*AS*174	Thermocouple in space defined by Columns A and B, Rows 4 and 5.			34, 327	
TFV*RS*126	Thermocouple in space defined by Columns B and C, Rows 3 and 4.			35, 328	
<u>Grid Spacer 5</u>	330 cm below cold leg centerline, 166 cm above bottom of heated length.				
TFV*RS*166	Thermocouple in space defined by Columns B and C, Rows 3 and 4.			36, 329	
<u>Grid Spacer 7</u>	230 cm below cold leg centerline, 246 cm above bottom of heated length.				
TFV*RS*246	Thermocouple in space defined by Columns B and C, Rows 3 and 4.			37, 330	
<u>Grid Spacer 8</u>	210 cm below cold leg centerline, 286 cm above bottom of heated length.				
TFV*AA*286	Thermocouple in space defined by Columns A and B, Rows 4 and 5.			38, 331	
<u>Grid Spacer 9</u>	170 cm below cold leg centerline, 326 cm above bottom of heated length.				
TFV*RS*326	Thermocouple in space defined by Columns B and C, Rows 3 and 4.			39, 332	
<u>Grid Spacer 10</u>	130 cm below cold leg centerline, 366 cm above bottom of heated length.				
TFV*AA*366	Thermocouple in space defined by Columns A and B, Rows 4 and 5.			40, 333	
<u>Steam Generator</u>		0 to 1533 K	0 to 82° K		
<u>Intact Loop, Primary Side</u>	Between Spools 7 and 8.				
TFIP*LR30	In long tube, hot side, 30 cm above top of tube sheet.			41, 334	
TFIP*LR84	In long tube, hot side, 84 cm above top of tube sheet.			42, 335	
TFIP*LR152	In long tube, hot side, 152 cm above top of tube sheet.			63	Failed during S-SF-5
TFIP*LR452	In long tube, hot side, 452 cm above top of tube sheet.			44, 336	
TFIP*SR815	In short tube, hot side, 815 cm above top of tube sheet.			45, 337	
TFIP*LR922	In long tube, hot side, 922 cm above top of tube sheet.			46, 338	
TFIP*LC785	In long tube, cold side, 785 cm above top of tube sheet.			47, 339	
TFIP*SC668	In short tube, cold side, 668 cm above top of tube sheet.			48, 340	
TFIP*LC333	In long tube, cold side, 333 cm above top of tube sheet.			49, 341	
TFIP*LC*11	In long tube, cold side, 211 cm above top of tube sheet.			50, 342	
TFIP*SC211	In short tube, cold side, 211 cm above top of tube sheet.			51, 343	

Table 5. (continued)

Measurement	Location and Comments ^a	Data Acquisition Range ^a		Figure ^a	Measurement Comments ^b
		Detector	System		
FLUID TEMPERATURE (continued)					
<u>Broken Loop, Primary Side</u>					
	Nerecan Spools 59 and 60.	0 to 1533 K	0 to 820 K		
TFBP+LR152	In long tube, hot side, 152 cm above top of tube sheet.			52, 344	
TFBP+SR211	In short tube, hot side, 211 cm above top of tube sheet.			53, 345	
TFBP+LR211	In long tube, hot side, 211 cm above top of tube sheet.			54, 346	
TFBP+LR272	In long tube, hot side, 272 cm above top of tube sheet.			55, 347	
TFBP+LR394	In long tube, hot side, 394 cm above top of tube sheet.			56, 348	
TFBP+LR452	In long tube, hot side, 452 cm above top of tube sheet.			57, 349	
TFBP+LR785	In long tube, hot side, 785 cm above top of tube sheet.			58, 350	
TFBP+LR922	In long tube, hot side, 922 cm above top of tube sheet.			59, 351	
TFBP+LC785	In long tube, cold side, 785 cm above top of tube sheet.			60, 352	
TFBP+SC452	In short tube, cold side, 452 cm above top of tube sheet.			61, 353	
TFBP+LC452	In long tube, cold side, 452 cm above top of tube sheet.			62, 354	
TFBP+LC211	In long tube, cold side, 211 cm above top of tube sheet.			63, 355	
<u>Intact Loop, Secondary Side</u>					
		0 to 1533 K	0 to 820 K		
TFSC+IGFDW	Feedwater temperature at flow orifice.			64, 356	
TFSC+IGFWL	Feedwater temperature at lower injection port.			65, 357	
TFSC+IAXFW	Auxiliary feedwater at entrance to upper feed ring.			66, 358	
TFIS*D+152	In downcomer, 152 cm above top of tube sheet.			67, 359	
TFIS*D+457	In downcomer, 457 cm above top of tube sheet.			68, 360	
TFIS*D+609	In downcomer, 609 cm above top of tube sheet.			69	Test S-SF-5 only
TFIS*D+761	In downcomer, 761 cm above top of tube sheet.			65, 362	
TFIS+LR30	On long tube, hot side, 30 cm above top of tube sheet.			70, 363	
TFIS+LC30	On long tube, cold side, 30 cm above top of tube sheet.			71	Failed during S-SF-5
TFIS+SR84	On short tube, hot side, 84 cm above top of tube sheet.			72, 364	
TFIS+LR84	On long tube, hot side, 84 cm above top of tube sheet.			73, 365	
TFIS+LC84	On long tube, cold side, 84 cm above top of tube sheet.			74, 366	
TFIS+LR152	On long tube, hot side, 152 cm above top of tube sheet.			75, 367	
TFIS+LC211	On long tube, cold side, 211 cm above top of tube sheet.			76, 368	
TFIS+LC333	On long tube, cold side, 333 cm above top of tube sheet.			77, 369	

Table 5. (continued)

Measurement	Location and Comments ^a	Data Acquisition Range ^a		Figure ^a	Measurement Comments ^b
		Detector	System		
FLUID TEMPERATURE (continued)					
<u>Intact Loop,</u> <u>Secondary Side</u> (continued)					
TFIS*SC333	On short tube, cold side, 333 cm above top of tube sheet.			78, 370	
TFIS*LN394	On long tube, hot side, 394 cm above top of tube sheet.			79, 371	
TFIS*SH452	On short tube, hot side, 452 cm above top of tube sheet.			80, 372	
TFIS*LN452	On long tube, hot side, 452 cm above top of tube sheet.			81, 373	
TFIS*LC452	On long tube, cold side, 452 cm above top of tube sheet.			82, 374	
TFIS*LN785	On long tube, hot side, 785 cm above top of tube sheet.			83, 375	
TFIS*1117	In steam dome, 1117 cm above top of tube sheet.			84, 376	
<u>Broken Loop,</u> <u>Secondary Side</u>					
		0 to 1533 K	0 to 820 K		
TFSC*SGFWL	Feedwater temperature at lower injection port.			85, 377	
TFSC*BAEPW	Auxiliary feedwater at entrance to upper feed ring.			86, 378	
TFBS*D+152	In downcomer, 152 cm above top of tube sheet.			87, 379	
TFBS*D+304	In downcomer, 304 cm above top of tube sheet.			88, 380	
TFBS*D+457	In downcomer, 457 cm above top of tube sheet.			89, 381	
TFBS*D+610	In downcomer, 610 cm above top of tube sheet.			90, 382	
TFBS*D+761	In downcomer, 761 cm above top of tube sheet.			91, 383	
TFBS*LN61	On long tube, hot side, 61 cm above top of tube sheet.			92, 384	
TFBS*LC84	On long tube, cold side, 84 cm above top of tube sheet.			93, 385	
TFBS*LN211	On long tube, hot side, 211 cm above top of tube sheet.			94, 386	
TFBS*LC211	On long tube, cold side, 211 cm above top of tube sheet.			95, 387	
TFBS*LN333	On long tube, hot side, 333 cm above top of tube sheet.			96, 388	
TFBS*SC333	On short tube, cold side, 333 cm above top of tube sheet.			97, 389	
TFBS*LC333	On long tube, cold side, 333 cm above top of tube sheet.			98, 390	
TFBS*LN394	On long tube, hot side, 394 cm above top of tube sheet.			99, 391	
TFBS*SH452	On short tube, hot side, 452 cm above top of tube sheet.			100, 392	
TFBS*LN452	On long tube, hot side, 452 cm above top of tube sheet.			101, 393	
TFBS*LC452	On long tube, cold side, 452 cm above top of tube sheet.			102, 394	
TFBS*LN536	On long tube, hot side, 536 cm above top of tube sheet.			103, 395	
TFBS*LN668	On long tube, hot side, 668 cm above top of tube sheet.			104, 396	

Table 5. (continued)

Measurement	Location and Comments ^a	Data Acquisition Range ^a		Figure ^a	Measurement Comments ^b
		Detector	System		
<u>FLUID TEMPERATURE</u> (continued)					
<u>Broken Loop, Secondary Side</u> (continued)					
TFBS*LC785	On long tube, cold side, 785 cm above top of tube sheet.			105, 397	
TFBS*SHR15	On short tube, hot side, 815 cm above top of tube sheet.			106, 398	
TFBS*LN922	On long tube, hot side, 922 cm above top of tube sheet.			107, 399	
TFBS*1117	In steam dome, 1117 cm above top of tube sheet.			108, 400	
<u>Pressurizer</u>					
TF*PRZ*132	In top of pressurizer, 132 cm above exit to surge line.	0 to 1533 K	0 to 820 K	109, 401	
TF*PRZ*73	In surge line, 73 cm below pressurizer exit.			110, 402	
TF*PRZ*13	In surge line at entrance to intact loop Spool 3.			111, 403	
<u>Break Nozzle</u>					
TFSC*IGSTM	In intact loop steam generator, upstream of break nozzle.	0 to 1533 K	0 to 820 K	112, 404	
TFSC*BGSTM	In broken loop steam generator, upstream of break nozzle.			113, 405	
<u>Break Effluent Condensate System</u>					
TF*CT1*0	In bottom of condensate Catch Tank 1, zero cm above drain outlet.			114, 406	
TF*CT2*0	In bottom of condensate Catch Tank 2, zero cm above drain outlet.			115, 407	
TF*BCCON*0	In break effluent line at outlet of condensing coils.			116, 408	
TFIC*SRIN	Cooling water supply at inlet to condensing coils.			117, 409	
TFIC*SBOUT	Cooling water at outlet of condensing coils.			118, 410	
<u>METAL TEMPERATURE</u> Chromel-Alumel thermocouples unless specified otherwise.					
<u>Vessel</u> Internals.					
TMV*FPD*79	In vessel on upper plenum filler piece, 79 cm above cold leg centerline at 45°.	0 to 1533 K	0 to 820 K	119, 411	
TMV*FPF221	In vessel on upper head filler piece, 221 cm above cold leg centerline at 15°.			120, 412	
TMV*TS0221	In vessel on thermal shield, 221 cm above cold leg centerline at 225°.			121, 413	
<u>Intact Loop, Steam Generator</u>					
TMIG*LN452	On long tube, hot (inlet) side of D-tubes, 452 cm above top of tube sheet.	0 to 1533 K	0 to 820 K	122, 414	
<u>Broken Loop, Steam Generator</u>					
TMBC*LC84	On long tube, cold (outlet) side of D-tubes, 84 cm above top of tube sheet.	0 to 1533 K	0 to 820 K	123, 415	
TMBC*LN452	On long tube, hot (inlet) side of D-tubes, 452 cm above top of tube sheet.			124, 416	

Table 5. (continued)

Measurement	Location and Comments ^a	Data Acquisition Range ^b		Figure ^c	Measurement Comments ^d
		Detector	System		
METAL TEMPERATURE (continued)					
<u>External Heaters</u>	Thermocouples on pipe outside surface under an external heat plate.	0 to 1533 K	0 to 820 K		
<u>Intact Loop</u>					
TMEH*16	Pump suction leg, Spool 16, 542 cm from downcomer center.			125, 417	
TMEH*17	Pump suction leg, Spool 17, 402 cm from downcomer center.			126	Failed during S-SF-5
TMEH*22	Cold leg, Spool 21, 42 cm from downcomer center.			127, 418	
<u>Broken Loop</u>					
TMEH*71V	Pump suction leg, Spool 72, middle, 465 cm from downcomer center.	0 to 1533 K	0 to 820 K	128, 419	
TMEH*73	Pump suction leg, Spool 73, 321 cm from downcomer center.			129, 420	
<u>Vessel</u>					
TMEH*V-196	Core housing, 196 cm below cold leg centerline.	0 to 1533 K	0 to 820 K	130, 421	
TMEH*V-30	Upper plenum, 30 cm below cold leg centerline.			131, 422	
MATERIAL TEMPERATURE					
<u>External Heaters</u>	Thermocouples on external heater outside surface, under insulation.	0 to 1533 K	0 to 820 K		
<u>Intact Loop</u>					
TEH*3	Hot leg, Spool 3, 174 cm from vessel center.			132, 423	
TEH*7	Hot leg, Spool 7, 447 cm from vessel center.			133, 424	
TEH*8	Cold leg, Spool 8, 1082 cm from downcomer center.			134, 425	
TEH*13	Cold leg, Spool 13, 798 cm from downcomer center.			426	Failed during S-SF-4
TEH*16	Cold leg, Spool 16, 542 cm from downcomer center.			135, 427	
TEH*17	Cold leg, Spool 17, 402 cm from downcomer center.			136, 428	
TEH*19	Cold leg, Spool 19, 243 cm from downcomer center.			137, 429	
TEH*22	Cold leg, Spool 22, 42 cm from downcomer center.			430	Failed during S-SF-4
<u>Broken Loop</u>					
TEH*50	Hot leg, Spool 50, 6 cm from vessel center.	0 to 1533 K	0 to 820 K	138, 431	
TEH*55A	Hot leg, Spool 55, 240 cm from vessel center.			139, 432	
TEH*59	Hot leg, Spool 59, 389 cm from vessel center.			140, 433	
TEH*60	Cold leg, Spool 60, 1042 cm from downcomer center.			141, 434	
TEH*64T	Cold leg, Spool 64, top, 885 cm from downcomer center.			142, 435	
TEH*64M	Cold leg, Spool 64, middle, 764 cm from downcomer center.			143, 436	
TEH*64B	Cold leg, Spool 64, bottom, 662 cm from downcomer center.			144, 437	
TEH*72M	Cold leg, Spool 72, middle, 405 cm from downcomer center.			145, 438	

Table 5. (continued)

Measurement	Location and Comments ^a	Data Acquisition Range ^a		Figure ^a	Measurement Comments ^b
		Detector	System		
MATERIAL TEMPERATURE (continued)					
<u>Broken Loop</u> (continued)					
TEMP73	Cold leg, Spool 73, 321 cm from downcomer center.			146, 439	
TEMP74	Cold leg, Spool 74, 196 cm from downcomer center.			147, 440	
TEMP79	Cold leg, Spool 79, 98 cm from downcomer center.			148, 441	
<u>Vessel</u>					
TEMPD-237	On downcomer, 237 cm below cold leg centerline.	0 to 1533 K	0 to 820 K	149, 442	
TEMPV-360	Core housing, 360 cm below cold leg centerline.			150, 443	
TEMPV-196	Core housing, 196 cm below cold leg centerline.			151, 444	
TEMPV-30	Upper plenum, 30 cm below cold leg centerline.			152, 445	
TEMPV+101	Upper plenum, 101 cm above cold leg centerline.			153, 446	
TEMPV+249	Upper head, 249 cm above cold leg centerline.			154, 447	
TEMPV+386	Upper head, 386 cm above cold leg centerline.			155, 448	
CORE HEATER Thermocouples located inside sheath of electric core heater rods.					
CLADDING TEMPERATURE					
<u>High Power Bus Heaters</u>					
	Nine rods in center of core.	0 to 1533 K	0 to 1580 K		
THV#B3+110	Heater at Column B, Row 3, thermocouples 114 cm (97"), 180 cm (353"), and 229 cm (304") above bottom of heated length.			156, 449	
THV#B3+184				157, 450	
THV#B3+229				158, 451	
THV#B4+140	Heater at Column B, Row 4, thermocouple at 140 cm (228") and above bottom of heated length.			159, 452	
THV#C2+137	Heater at Column C, Row 2, thermocouple at 137 cm (351") above bottom of heated length.			160, 453	
THV#C3+140	Heater at Column C, Row 3, thermocouple at 140 cm (174") above bottom of heated length.			161, 454	
THV#C4+167	Heater at Column C, Row 4, thermocouples at 162 cm (171") and 187 cm (182") above bottom of heated length.			162, 455	
THV#C4+187				163, 456	
THV#D2+16	Heater at Column D, Row 2, thermocouples at 16 cm (115"), 234 cm (351"), and 321 cm (270") above bottom of heated length.			164, 457	
THV#D2+254				165, 458	
THV#D2+321				166, 459	
THV#D3+109	Heater Column D, Row 3, thermocouple at 109 cm (217") above bottom of heated length.			167, 460	
THV#D4+179	Heater at Column D, Row 4, thermocouple at 179 cm (26"), above bottom of heated length.			168, 461	
<u>Low Power Bus Heaters</u>					
	Sixteen rods on periphery of core bundle.	0 to 1533 K	0 to 1580 K		
THV#A1+115	Heater at Column A, Row 1, thermocouple at 115 cm (126") above bottom of heated length.			169	Failed during S-SP-5
THV#A2+353	Heater at Column A, Row 2, thermocouple at 353 cm (180") above bottom of heated length.			170, 462	

Table 5. (continued)

Measurement	Location and Comments ^a	Data Acquisition Range ^a		Figure ^a	Measurement Comments ^b
		Detector	System		
CORE HEATER					
CLADDING TEMPERATURE					
(continued)					
<u>Low Power</u>					
<u>Bus Heaters</u>					
(continued)					
THVA3+76	Heater at Column A, Row 3,			171, 463	
THVA3+157	thermocouples at 76 cm (232"),			172, 464	
THVA3+208	157 cm (18"), 208 cm (121"),			173, 465	
THVA3+228	228 cm (174"), and 291 cm (230") from			174, 466	
THVA3+291	bottom of heated length.			175, 467	
THVA1+183	Heater at Column A, Row 1,			176, 468	
THVA1+253	thermocouples at 183 cm (173") and			177, 469	
	253 cm (1") above bottom of				
	heated length.				
THVC1+79	Heater at Column C, Row 1,			178, 470	
THVC1+211	thermocouples at 79 cm (291")			179, 471	
THVC1+292	211 cm (212") and 292 cm (0")			180, 472	
	above bottom of heated length.				
THVC5+133	Heater at Column C, Row 5,			181, 473	
THVC5+228	thermocouples at 133 cm (180")			182, 474	
	and 228 cm (70") above bottom of				
	heated length.				
THVD1+131	Heater at Column D, Row 1,			183, 475	
	thermocouple at 131 cm (60") above				
	bottom of heated length.				
THVE2+109	Heater at Column E, Row 2,			184, 476	
THVE2+181	thermocouples at 109 cm (117") and			185, 477	
	181 cm (67") above bottom of heated				
	length.				
THVE3+211	Heater at Column E, Row 3,			186, 478	
	thermocouple at 211 cm (45") above				
	bottom of heated length.				
THVE5+227	Heater at Column E, Row 5,			187, 479	
	thermocouple at 227 cm (45") above				
	bottom of heated length.				
PRESSURE					
<u>Intact Loop</u>					
P1+1	Hot leg, Spool 1, 60 cm from vessel	0 to 17.24 MPa	0 to 21.96 MPa	188, 480	
	center.				
<u>Broken Loop</u>					
PB+50	Hot leg, Spool 50, 74 cm from vessel	0 to 17.24 MPa	0 to 21.89 MPa	189, 481	
	center.				
PB+79	Cold leg, Spool 79, 96 cm from	0 to 17.24 MPa	0 to 21.72 MPa	190, 482	
	downcomer center.				
<u>Vessel</u>					
PV+UP-13	In core vessel upper plenum, 13 cm	0 to 17.24 MPa	0 to 21.64 MPa	191, 483	
	below cold leg centerline.				
PV+UR+421	In core vessel upper head, 421 cm	0 to 17.24 MPa	0 to 20.26 MPa	192, 484	
	above cold leg centerline.				
<u>Intact Loop</u>					
<u>Steam Generator</u>					
PIS+1117	In steam dome, 1117 cm above top of	0 to 6.90 MPa	0 to 8.722 MPa	193, 485	
	tube sheet.				
<u>Broken Loop</u>					
<u>Steam Generator</u>					
PBS+1117	In steam dome, 1117 cm above top of	0 to 6.90 MPa	0 to 8.304 MPa	194, 486	
	tube sheet.				
<u>Pressurizer</u>					
P+PRZ+158	In pressurizer steam dome, 158 cm	0 to 17.24 MPa	0 to 22.84 MPa	195, 487	
	above exit to surge line.		0 to 20.66 MPa		

Table 5. (continued)

Measurement ^a	Location and Comments ^a	Data Acquisition Range ^a		Figure ^a	Measurement Comments ^b
		Detector	System		
<u>PRESSURE (continued)</u>					
<u>Intact Loop Steam Generator</u>					
PSC*IGSTM	Steam exhaust. In steam discharge line, at flow orifice.	0 to 17.24 MPa	0 to 20.49 MPa	196, 488	
<u>Broken Loop Steam Generator</u>					
PSC*BGSTM	Steam exhaust. In steam discharge line, at flow orifice.	0 to 17.74 MPa	0 to 20.03 MPa	197, 489	
<u>Condensate System</u>					
PSC*BGCON	Broken loop effluent downstream of break valve at entrance to condensing coils.	0 to 3.45 MPa	0 to 3.44 MPa	198, 490	
<u>Cooling Water</u>					
PIC*SRFR	In supply line at entrance to condensing coils.	0 to 0.69 MPa	0 to 0.688 MPa	199, 491	
<u>DIFFERENTIAL PRESSURE</u>					
Elevation difference between transducer taps is zero and cells read zero when full cold, at no flow, unless specified otherwise. Cell positive (high pressure) side is plumbed to the first tap designated by the measurement alphanumeric name.					
<u>Intact Loop</u>					
D-V13A*15	Vessel upper plenum, 13 cm (0") below cold leg centerline, to hot leg, Spool 5, 347 cm from vessel center. Spool 5 tap is 96 cm above upper plenum tap.	±124.4 kPa	±168.3 kPa	492	Failed during S-SF-4
DPI*5A6	Hot leg, Spool 5, 347 cm from vessel center, to cold leg, Spool 9, 1030 cm from downcomer center across the intact loop steam generator primary tubes. Spool 9 tap is 16 cm above Spool 5 tap.	±344.75 kPa	±342.4 kPa	200, 493	
DPI*9K14	Cold leg, Spool 9, 1030 cm from downcomer center, to cold leg, Spool 14, 655 cm from downcomer center. Spool 9 tap is 355 cm above Spool 14 tap.	±344.75 kPa	±345.2 kPa	201, 494	
DPI*14*18	Cold leg, Spool 14, 655 cm from downcomer center, to cold leg, Spool 18, 325 cm from downcomer center. Spool 18 tap is 210 cm above Spool 14 tap.	±174.61 kPa	±102.0 kPa	202, 495	
DPI*21*18	Cold leg, Spool 21, Tap B, 127 cm from downcomer center to cold leg, Spool 18, Tap B, 325 cm from downcomer center, across intact loop pump. Spool 21 tap is 25 cm above Spool 18 tap.	±689.5 kPa	±690.1 kPa	203, 496	
D*1214*029	Cold leg, Spool 21, 127 cm from downcomer center to vessel downcomer, 29 cm above cold leg centerline. Vessel downcomer tap is 29 cm above Spool 21 tap.	±24.87 kPa	±33.73 kPa	204, 497	
<u>Broken Loop</u>					
D-V13A*57	Vessel upper plenum, 13 cm (0") below cold leg centerline, to hot leg, Spool 57, 306 cm from vessel center. Spool 57 tap is 93 cm above upper plenum tap.	±174.61 kPa	±99.98 kPa	205, 498	
DPI*57*62	Hot leg, Spool 57, 306 cm from vessel center, to cold leg, Spool 62, 947 cm from downcomer center, across broken loop steam generator primary tubes. Spool 62 tap is 9 cm above Spool 57 tap.	±689.5 kPa	±689.1 kPa	206, 499	

Table 5. (continued)

Measurement	Location and Comments ^a	Data Acquisition Range ^a		gure ^a	Measurement Comments ^b
		Detector	System		
<u>DIFFERENTIAL PRESSURE</u> (continued)					
<u>Broken Loop</u> (continued)					
DPB*62*65	Cold leg, Spool 62, 967 cm from downcomer center, to cold leg, Spool 65, 566 cm from downcomer center. Spool 62 tap is 370 cm above Spool 65 tap.	±174.61 kPa	±104.3 kPa	207, 500	
DPB*65*73	Cold leg, Spool 65, 566 cm from downcomer center, to cold leg, Spool 73, 341 cm from downcomer center. Spool 73 tap is 233 cm above Spool 65 tap.	±174.61 kPa	±101.3 kPa	208, 501	
DPB*74*73	Cold leg, Spool 74, Tap K, 202 cm from downcomer center, to cold leg, Spool 73, 341 cm from downcomer center, across broken loop pump. Spool 74 tap is 70 cm above Spool 73 tap.	±1379 kPa	±1379 kPa	209, 502	
DPB*74*VD29	Cold leg, Spool 74, 202 cm from downcomer center, to vessel downcomer, 29 cm above cold leg centerline. Vessel downcomer tap is 29 cm above Spool 74 tap.	±124.35 kPa	±170.3 kPa	210, 503	
<u>Vessel</u>					
DVD*29*160	Vessel downcomer, 29 cm above cold leg centerline, to vessel upper head, 160 cm above cold leg centerline, across the downcomer to upper head bypass line. Upper head tap is 131 cm above downcomer tap.	±344.75 kPa	±344.8 kPa	211, 504	
<u>Intact Loop Steam Generator</u>					
Secondary side.					
DPSC*IGFDW	Across flow orifice in feedwater supply line.	±198.96 kPa	±348.16 kPa	212, 505	
DPSC*IGSTM	Across flow orifice in steam exhaust line.	±198.96 kPa	±348.16 kPa	213	Test S-SF-4 only
<u>Broken Loop Steam Generator</u>					
Secondary side.					
DPSC*BCFDW	Across flow orifice in feedwater supply line.	±174.35 kPa	±217.61 kPa	214, 506	
DPSC*BCSTM	Across flow orifice in steam exhaust line.	±138.53 kPa	±262.47 kPa	215	Test S-SF-4 only
<u>Pressurizer</u>					
DP*PRZ*13C	In surge line, from 25 cm above pressurizer outlet, to surge line inlet, to intact loop hot leg, Spool 3, Port C. Pressurizer tap is 157 cm above Spool 3 tap.	±3447.5 kPa	±3445. kPa	216, 507	
<u>Steam Line Break Assembly</u>					
DPSC*SLB1	From broken loop steam generator steam dome, Port D (1117 cm), to upstream of break orifice.	±344.7 kPa	±344.8 kPa	217, 508	
DPSC*SLB2	Across broken loop break orifice.	±6895 kPa	±9169 kPa	218, 509	
DPSC*SLB3	From intact loop steam generator steam dome, Port D (1117 cm), to upstream of break orifice.	±344.7 kPa	±344.9 kPa	219, 510	
DPSC*---	Across intact loop break orifice.	±6895 kPa	±9274 kPa	220, 511	
DPIC*SRPB	Across flow orifice in cooling water line to condensate coils.	±74.61 kPa	±100.7 kPa	221, 512	

Table 5. (continued)

Measurement	Location and Comments ^a	Data Acquisition Range ^a		Figure ^c	Measurement Comments ^b
		Detector	System		
LIQUID LEVEL					
Transducers read zero when system is full and, at no flow, unless specified otherwise. Cell positive (high pressure) side is plumbed to the first tap designated by the measurement alphanumeric name.					
<u>Vessel</u>					
LV+29-578	Vessel downcomer, 29 cm above cold leg centerline, to vessel lower plenum, 578 cm below cold leg centerline. Tap elevation difference is 607 cm.	±346.75 kPa	±343.2 kPa	222, 513	
LV+136-578	Vessel upper plenum, 13 cm (180°) below cold leg centerline, to vessel lower plenum, 578 cm below cold leg centerline. Tap elevation difference is 565 cm.	±124.35 kPa	±176.1 kPa	223, 514	
LV+105-501	Vessel core housing, 105 cm below cold leg centerline, to vessel lower plenum, 501 cm below cold leg centerline. Tap elevation difference is 396 cm.	±74.61 kPa	±101.3 kPa	224, 515	
LV+160-13M	Vessel upper head, 160 cm above cold leg centerline, to vessel upper plenum, 13 cm (180°) below cold leg centerline. Tap elevation difference is 173 cm.	±24.87 kPa	±33.09 kPa	225, 516	
LV+421+160	Vessel upper head, 421 cm to 160 cm above cold leg centerline. Tap elevation difference is 261 cm.	±24.87 kPa	±33.60 kPa	226, 517	
<u>Intact Loop Steam Generator</u>					
Level of primary fluid inside vertical U-tubes.					
LI1838-578	In short tube, hot side of apex, at 838 cm above top of tube sheet, to entrance plenum, 57 cm below top of tube sheet. Tap elevation difference is 895 cm.	±198.96 kPa	±266 kPa	227, 518	
LI1905-578	In medium tube, hot side of apex, at 905 cm above top of tube sheet, to entrance plenum, 57 cm below top of tube sheet. Tap elevation difference is 962 cm.	±124.35 kPa	±167.6 kPa	228, 519	
LI1971-578	In long tube, hot side of apex, at 971 cm above top of tube sheet, to entrance plenum, 57 cm below top of tube sheet. Tap elevation difference is 1028 cm.	±124.35 kPa	±170.2 kPa	229, 520	
<u>Intact Loop Steam Generator</u>					
Level of secondary fluid in downcomer and riser sections.					
LI18117+50	From steam dome at 1117 cm, to downcomer at 50 cm, above top of tube sheet.	±346.75 kPa	±344.2 kPa	230, 521	
LI11178825	From steam dome at 1117 cm, to downcomer at 825 cm, above top of tube sheet.	±74.61 kPa	±115.2 kPa	231, 522	
LI11178836	From steam dome at 1117 cm, to riser at 836 cm, above top of tube sheet.	±74.61 kPa	±105.9 kPa	232, 523	
LI1836+463	From riser at 836 cm, to riser at 463 cm, above top of tube sheet.	±74.61 kPa	±100.1 kPa	233, 524	
LI18+63+89	From riser at 463 cm, to riser at 89 cm, above top of tube sheet.	±74.61 kPa	±102.3 kPa	234, 525	
LI18+89+50	From riser at 89 cm, to downcomer at 50 cm, above top of tube sheet. Across flow shutter.	±12.43 kPa	±18.51 kPa	235, 526	
<u>Broken Loop Steam Generator</u>					
Level of primary fluid inside vertical U-tubes.					
LI1838-578	In short tube, hot side of apex, at 838 cm above top of tube sheet, to entrance plenum, 57 cm below top of tube sheet. Tap elevation difference is 895 cm.	±124.35 kPa	±170.3 kPa	236, 527	

Table 5. (continued)

Measurement	Location and Comments ^a	Data Acquisition Range ^a		Figure ^a	Measurement Comments ^b
		Detector	System		
<u>LIQUID LEVEL</u> (continued)					
<u>Broken Loop Steam Generator (continued)</u>					
LBS1117+50	From steam dome at 1117 cm, to downcomer at 50 cm, above top of tube sheet.	†124.35 kPa	†159.8 kPa	237, 528	
LBS1117+825	From steam dome at 1117 cm to downcomer at 825 cm, above top of tube sheet.	†124.35 kPa	†158.8 kPa	238, 529	
LBS1117+836	From steam dome at 1117 cm, to riser at 836 cm, above top of tube sheet.	†74.61 kPa	†107.6 kPa	239, 530	
LBS836+463	From riser at 836 cm, to riser at 463 cm, above top of tube sheet.	†124.35 kPa	†170.2 kPa	240, 531	
LBS+825+50	From downcomer at 825 cm, to downcomer at 50 cm, above top of tube sheet.	†124.35 kPa	†168.2 kPa	241, 532	
LBS+463+89	From riser at 463 cm, to riser at 89 cm, above top of tube sheet.	†74.61 kPa	†101.1 kPa	242, 533	
LBS+89+50	From riser at 89 cm, to downcomer at 50 cm, above top of tube sheet. Across flow shutter.	†24.87 kPa	†34.79 kPa	243, 534	
<u>Pressurizer</u>					
LPW2146+25	From steam dome at 146 cm, to bottom at 25 cm, above pressurizer outlet to surge line.	†12.43 kPa	†16.73 kPa	244, 535	Trend data only
<u>Condensate Tanks</u>					
L1CT23+462	Level in Condensate Tank 1, from 23 cm to 462 cm above the tank bottom drain line.	†68.95 kPa	†92.35 kPa	245, 536	
L2CT23+462	Level in Condensate Tank 2, from 23 cm to 462 cm above the tank bottom drain line.	†68.95 kPa	†92.76 kPa	246, 537	
<u>Feedwater Tank</u>					
L1CT488+97	Level in feedwater tank, from 97 cm to 488 cm above tank inlet flange.	†37.57 kPa	†37.6 kPa	247, 538	
<u>VOLUMETRIC FLOW RATE</u>					
<u>Intact Loop</u>					
Primary coolant.					
Q1*1	Hot leg at Spool 1, 38 cm from vessel center.	†1.9 to 19 L/s	†14 L/s	248, 539	
Q1*15	Cold leg at Spool 15, 629 cm from downcomer center.	†5.6 to 56 L/s	†14 L/s	249	Failed during S-SF-5
Q1*21	Cold leg at Spool 21, 151 cm from downcomer center.	†1.9 to 15 L/s	†14 L/s	250, 540	
<u>Broken Loop</u>					
Primary coolant.					
Q8*50	Hot leg at Spool 50, 100 cm from vessel center.	†1.3 to 12.6 L/s	†6.0 L/s	251	Failed during S-SF-5
Q8*57	Hot leg at Spool 57, 200 cm from vessel center.	†1.3 to 12.7 L/s	†6.0 L/s	252	Failed during S-SF-5
Q8*73	Cold leg at Spool 73, 305 cm from downcomer center.	†1.25 to 12.5 L/s	†6.0 L/s	541	Test S-SF-5 only
Q8*79	Cold leg at Spool 79, 110 cm from downcomer center.	†1.25 to 12.5 L/s	†5.0 L/s	253, 542	
<u>Vessel</u>					
QV*DC-423	Vessel downcomer, 423 cm below cold leg centerline.	†1.5 to 15 L/s	†19 L/s	254, 543	

Table 5. (continued)

Measurement	Location and Comments ^a	Data Acquisition Gauge ^a		Figure ^a	Measurement Comments ^b
		Detector	System		
VOLUMETRIC FLOW RATE (continued)					
<u>Vessel</u> (continued)					
QV*GT+321	In vessel guide tube at 321 cm above the cold leg centerline.	±0.035 to 0.35 L/s	±2.5 L/s	255, 544	
QV*BYPASS	In vessel downcomer to upper head bypass line.	±0.07 to 0.7 L/s	±3.0 L/s	256, 545	
<u>Pressurizer</u>					
QV*PRZ-30	Primary coolant. In pressurizer surge line, 30 cm from pressurizer exit. Positive reading indicates an outsurge from the pressurizer.	±0.32 to 3.2 L/s	±3.0 L/s	257, 546	
<u>Auxiliary Feedwater</u>					
QSC*IGAXFW	Emergency secondary coolant. In discharge line of intact loop steam generator, auxiliary feedwater supply pump.	±0.0064 to 0.064 L/s	±0.0624 L/s	258, 547	
QSC*BGAXFW	In discharge line of broken loop steam generator, auxiliary feedwater supply pump.	±0.0051 to 0.051 L/s	±0.0503 L/s	259, 548	
QCI*1LHPIS	In line leading from high pressure injection pump for intact loop.	±0.0157 to 0.157 L/s	±0.30 L/s	260, 549	
DENSITY					
<u>Intact Loop</u>					
RI*SM	Primary coolant. Horizontal beam through the middle of hot leg vertical Spool 5 at entrance to steam generator.	1.6 to 1600 kg/m ³	0 to 1600 kg/m ³	261, 550	
<u>Broken Loop</u>					
RI*SM	Primary coolant. Horizontal beam through the middle of hot leg vertical Spool 57 at entrance to steam generator.	1.6 to 1600 kg/m ³	0 to 1600 kg/m ³	262, 551	
<u>Vessel</u>					
RV*DC-72	Primary coolant. Vessel downcomer, 72 cm below cold leg centerline.	1.6 to 1600 kg/m ³	0 to 1600 kg/m ³	263, 552	
RV*DC-260	Vessel downcomer, 260 cm below cold leg centerline.	1.6 to 1600 kg/m ³	0 to 1600 kg/m ³	264, 553	
RV*DC-456	Vessel downcomer, 456 cm below cold leg centerline.	1.6 to 1600 kg/m ³	0 to 1600 kg/m ³	265, 554	
RV*AB-6	6 cm below bottom of core heated length, 502 cm below cold leg centerline, between heater rod Columns A and B.	1.6 to 1600 kg/m ³	0 to 1600 kg/m ³	266, 555	
RV*23+13	13 cm above bottom of core heated length, 483 cm below cold leg centerline, between heater rod Rows 2 and 3.	1.6 to 1600 kg/m ³	0 to 1600 kg/m ³	267, 556	
RV*23+113	113 cm above bottom of core heated length, 383 cm below cold leg centerline, between heater rod Rows 2 and 3.	1.6 to 1600 kg/m ³	0 to 1600 kg/m ³	268, 557	
RV*AB+173	173 cm above bottom of core heated length, 323 cm below cold leg centerline, between heater rod Columns A and B.	1.6 to 1600 kg/m ³	0 to 1600 kg/m ³	269, 558	
RV*23+183	183 cm above bottom of core heated length, 313 cm below cold leg centerline, between heater rod Rows 2 and 3.	1.6 to 1600 kg/m ³	0 to 1600 kg/m ³	270, 559	
RV*23+253	253 cm above bottom of core heated length, 243 cm below cold leg centerline, between heater rod Rows 2 and 3.	1.6 to 1600 kg/m ³	0 to 1600 kg/m ³	271, 560	

Table 5. (continued)

Measurement	Location and Comments ^a	Data Acquisition Range ^a		Figure ^a	Measurement Comments ^b
		Detector	System		
DENSITY (continued)					
<u>Vessel (continued)</u>					
KV*23+342	342 cm above bottom of core heated length, 153 cm below cold leg centerline, between heater rod Rows 2 and 3.			272, 561	
KV*09+11	In vessel at base of core flow instrument bays, 11 cm below cold leg centerline.			273, 562	
KV*09+173	In vessel upper head, 173 cm above cold leg centerline.			274, 563	
KV*09+339	In vessel upper head, 339 cm above cold leg centerline.			275, 564	
CORE POWER CHARACTERISTICS					
<u>High Power Bus</u>					
Nine rods on center of core bundle.					
IV*HWPBUS	Total current from high power bus power supplies.	0 to 10000 A	0 to 5000 A	276, 565	
EV*HWPBUS	Total voltage from high power bus power supplies.	0 to 400 V	0 to 499.75 V	277, 566	
<u>Low Power Bus</u>					
Sixteen rods on periphery of core bundle.					
IV*LOWBUS	Total current from low power bus power supplies.	0 to 10,000 A	0 to 5000 A	278, 567	
EV*LOWBUS	Total voltage from low power bus power supplies.	0 to 400 V	0 to 499.75 V	279, 568	
<u>Calculated Power</u>					
Posttest calculations performed on recorded core voltage and current.					
KW*HIC	Total power on rods of the high power bus.			280, 569	
KW*LOC	Total power on rods of the low power bus.			281, 570	
KW*TOIC	Total power on all core rods.			282, 571	
<u>Power Supply 357</u>					
Core vessel and downcomer.					
IM*UNIT357	Heater current.	0 to 400 A	0 to 300 A	283, 572	
EM*UNIT357	Heater voltage.	0 to 250 V	0 to 250 V	284, 573	
KW*H*V357	Calculated power.			285, 574	
<u>Power Supply 358</u>					
Intact loop pump suction (Spools 13 through 16).					
IM*UNIT358	Heater current.	0 to 500 A	0 to 400 A	286, 575	
EM*UNIT358	Heater voltage.	0 to 200 V	0 to 250 V	287, 576	
KW*H*V358	Calculated power.			288, 577	
<u>Power Supply 359</u>					
Broken loop pump suction (Spools 64, 65, 72, 73).					
IM*UNIT359	Heater current.	0 to 150 A	0 to 200 A	289, 578	
EM*UNIT359	Heater voltage.	0 to 200 V	0 to 250 V	290, 579	
KW*H*V359	Calculated power.			291, 580	
<u>Power Supply 360</u>					
Intact and broken loop cold legs. (Spools 28, 21, 22, 74, 76, 79).					
IM*UNIT360	Heater current.	0 to 100 A	0 to 200 A	292, 581	
EM*UNIT360	Heater voltage.	0 to 200 V	0 to 250	293, 582	
KW*H*V360	Calculated power.			294, 583	

Table 5. (continued)

Measurement	Location and Comments ^a	Data Acquisition Range ^b		Figure ^a	Measurement Comments ^b
		Detector	Scale		
CORE POWER CHARACTERISTICS (continued)					
<u>Power Supply 361</u>					
	Intact and broken loop hot legs (Spool 1 through 12, and 50 through 66.)				
IPONIT361	Heater current.	0 to 200 A	0 to 150 A	295, 584	
EPONIT361	Heater voltage.	0 to 200 V	0 to 250 V	296, 585	
KWEPFIBRL	Calculated power.			297, 586	
PUMP CHARACTERISTICS					
<u>Intact Loop</u>					
IIPUMP	Pump motor current.	0 to 250 A	0 to 250 A	298, 587	
EIPUMP	Pump motor voltage.	0 to 502 V	0 to 502 V	299, 588	
WIAPUMP	Pump shaft angular velocity.	0 to 3820 rad/s	0 to 400 rad/s	300, 589	
<u>Broken Loop</u>					
WBAPUMP	Pump shaft angular velocity.	0 to 2618 rad/s	0 to 2618 rad/s	301, 590	
KWBAPUMP	Pump motor power.	0 to 82 kW	0 to 20 kW	302, 591	Trend data only
VALVE POSITION					
<u>Intact Loop</u>					
ESONICSTM	Secondary coolant valves.				
	Steam exhaust valve.	0 to 10 V	10 to 10 V	303, 592	Trend data only

a. Statements at the beginning of a measurement category regarding location and comments, range, and figure apply to all subsequent measurements within the given category unless specified otherwise.

b. Detectors subjected to overrange conditions during portions of the test were capable of withstanding those conditions without change in operating or measuring characteristics when the physical conditions were again within the detector range.

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