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DEBRIS BED CHARACTERIZATION AND THERMAL BEHAVIOR MODELS FOR SCDAP

NRC Research and for Technical Assistance Report

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DEBRIS BED CHARACTERIZATION AND THERMAL BEHAVIOR MODELS FOR SCDAP

1. INTRODUCTION

During a severe accident in a light water reactor (LWR), two general processes, either individually or in combination, are expected to result in disruption of the core. The first process is the progressive liquefaction of the core components and the subsequent redistribution and solidification of the liquefied materials. This process may result in a debris region of frozen masses. The second process is the extensive fragmentation of components along a coolant quench front due to rapid, quench-induced thermal shock of embritted components. This process may result in a debris region of loosely bound fragments.

The above two processes may drastically change the geometry of the core. For example, fragmentation of a 1-m length of the fuel rods in a pressurized water reactor fuel assembly into particles with an average diameter of 500 μ m would increase the contact surface between fuel and coolant by a factor of 50. Also, coolant pressure drop across a 0.5-m thick porous debris bed with a coolant flow rate of 0.5 kg/m² s and a specific surface area exposed to coolant of 8 x 10⁵ m⁻¹ would be a factor of 10⁵ greater than that of an intact (rod-like) bundle. Obviously, the constitutive relations (loss coefficients, heat fluxes, etc.) for models normally used to analyze core thermal-hydraulic behavior must be modified to analyze disrupted core regions with such significantly different characteristics.

The Severe Core Damage Analysis Package (SCDAP) computer code¹ is being developed to analyze severe disruption of LWR cores. The initial version of SCDAP will analyze disruption of only a single fuel bundle. The models which have been developed for SCDAP to describe debris region characteristics and thermal behavior are described in this report. The models treat both conglomerate, or cohesive, debris beds and rubble debris beds which are formed by the liquefaction/redistribution/solidification and fragmentation processes, respectively. The models serve the following functions:

- They define debris bed characteristics which include bed porosity, bed height, equivalent particle diameter, coolant pressure drop across the bed, and whether a rubble bed is in a packed or fluidized state.
- They calculate debris bed and coolant temperature distributions and the state of bed coolability.
- 3. They describe propagation of a molting front within a debris bed.

Because of the paucity of data on debris beds for LWRs, the models described herein are considered preliminary in nature. The models will be assessed when appropriate data become available and will be refined accordingly for incorporation in a latter version of SCDAP.

Section 2 describes the development of the debris region characterization and thermal behavior models. Section 3 describes the structure of the models and implementation of the models in SCDAP. Lastly, Section 4 presents results of the acceptance testing of the models.

2. MODEL DEVELOPMENT

The debris bed characterization and behavior models described herein are, in general, based on LWR and Liquid Metal Fast Breeder Reactor (LMFBR) experimental data, porous body thermal-hydraulic analysis, fluidized bed thermal-hydraulic analysis, and the Post Accident Heat Removal (PAHR) dryout heat flux analysis performed for LMFBRs. Because of the lack of an appropriate data base for developing models specifically for use in LWR severe accident analysis, the following assumptions were required during development of the models described herein. The assumptions are:

- Debris bed is homogenous and consists of particles which can be effectively treated as spheres.
- Within a debris bed, coolant flow is homogeneous with perfect mixing of the liquid and vapor phases.
- Melting of material within a debris bed is an equilibrium process such that no superheating occurs until all of the debris has melted. The melting proceeds with infinite axial heat conduction.

Because the models assume homogenous flow conditions within a debris bed, some additional modeling considerations will be involved when the models are interfaced with the non-homogeneous bundle thermal-hydraulic models to be included in SCDAP.

The debris bed characterization models are described first. Then, the debris bed thermal models are described. Finally, a discussion of the range of applicability of the several correlations used for the model development is given.

2.1 Debris Bed Characterization

The models described in this section characterize both the cohesive and rubble depris beds for subsequent thermal analysis by the models described in Section 2.2.

2.1.1 Cohesive Debris Bed

Formation of a cohesive debris region is considered by two sets of models in SCDAP. Component liquefaction and liquefied material flow and solidification are analyzed with the LIQSOL models.² The debris transition and propagation models¹ consider the damage state for each component and determine when a bundle region has been sufficiently disrupted so that a cohesive or rubble debris region analysis is more appropriate than an intact bundle region analysis. When the criteria for transition to a cohesive debris region analysis are satisfied, the debris transition and propagation models calculate the following information:

- Cohesive debris region height and elevation with respect to the fuel bundle
- The masses of the individual constituents of the debris bed (UO₂, Zr, ZrO₂, etc.)
- Surface area of debris exposed to coolant per unit volume of solid material in the region.

These data are used to characterize the cohesive debris bed for subsequent thermal behavior analysis.

Assuming that all available material in the cohesive debris region forms a homogeneous, porous body, the zero-porosity volume of the debris, V_c , is calculated as

$$V_{c} = \frac{M_{U}O_{2}}{P_{U}O_{2}} + \frac{M_{Z}rO_{2}}{P_{Z}rO_{2}} + \frac{M_{Z}r}{P_{Z}r} + \frac{M_{S}t}{P_{S}t} + \frac{M_{A}b}{P_{A}b}$$
(1)

where

 V_c = zero-porosity volume of cohesive debris bed (m³)

= mass of constituent X within the cohesive debris region (kg)

= density of constituent X within the cohesive debris region
 (kg/m³)

2)

(3)

constituent material: UO₂, Zr, ZrO₂, St (structural material), and Ab (control rod material).

Using V_{r} , the porosity of the debris bed is calculated as

$$c = 1 - \frac{V_c}{A_c H_c}$$

where

E.

MX

P X

X

e = porosity of cohesive debris bed
A_c = cross-sectional area of disrupted bundle region (m²)
H_c = height of cohesive debris region (m).

Coolant pressure drop across a cohesive debris bed is calculated using Ergun's correlation based on a fixed-bed pressure drop analysis.^{3,4} The correlation used is

$$\frac{\Delta P_{c}}{u_{0}H_{c}} = \alpha_{c}\mu + \beta_{c}G$$

where

 ΔP_{c} = pressure drop across the bed (Pa)

u = superficial velocity of the coolant measured on an empty tube basis (m/s) u = coolant viscosity (kg/m*s)

G = coolant mass flux (kg/m²·s)

$$c = 150 \frac{(1 * e_c)^2}{e_c^3} \frac{1}{D_c^2}$$

$$B_{\rm c} = 1.75 \frac{1-\epsilon_{\rm c}}{\epsilon_{\rm c}^3} \frac{1}{D_{\rm c}} \, .$$

The particle diameter in Equation (3) is usually obtained by direct measurement of particle sizes. However, for a cohesive debris bed an equivalent particle diameter, D_c , can be derived from the definition of the specific surface area and the assumption that the particles are spherical:

$$S_c = \frac{\text{surface area exposed to the fluid}}{\text{total volume of solid material}}$$

$$= \frac{\pi D_{c}^{2}}{\frac{\pi D_{c}^{3}}{6}} = \frac{6}{D_{c}}$$

or

$$D_c = \frac{6}{S_c}$$

(4)

where

S = surface area of debris exposed to coolant per unit volume of solid material in the region (m⁻¹)

 D_{c} = equivalent particle diameter (m).

P characterizes the diameter of the particles in the cohesive debris bed. This approach has been successfully applied to Equation (3) as described in Reference 5.

In Equation (3), α_{c} and β_{c} are constants characterizing the structure of the porous material; α_{c} is the viscous resistance coefficient, and β_{c} is the inertial resistance coefficient. A characteristic length, l_{c} , of the pore structure is calculated from the definition⁶

 $l_c = \frac{\beta_c}{\alpha_c}$

(5)

where 1 is expressed in units of meters. The characteristic length is used to determine the volumetric heat transfer coefficient for interfacial transport of thermal energy between the solid and coolant. This will be discussed in Section 2.2.3.

2.1.2 Rubble Debris Bed

The debris transition and propagation models discussed in the previous section also consider formation of a rubble debris bed which may result during reflooding if sufficient component oxidation (embrittlement) has occurred prior to reflood. As in the case of cohesive debris, the debris transition and propagation models calculate data which are required to characterize a rubble debris bed for subsequent thermal analysis. These data are:

- Rubble debris region height and elevation with respect to the fuel bundle
- 2. The masses of the individual constituents of the debris bed
- 3. The average particle size for the rubble debris bed.

Theoretical analyses of random packings of particles have been under development for the past several decades.^{7,8} Debbas and Rampf⁹ treated random packings of irregularly shaped particles with different size distributions by means of statistical methods. In a systematic assemblage of uniform spheres, the lossest (cubic) and highest possible packings (rhombohedral and face-centered cubic) correspond to porosities of 0.43 and 0.26, respectively. For the initial version of SCDAP, the models which describe the thermal-hydraulic behavior of a rubble debris bed are based on the assumption of no variation in particle size along the axial direction of the bed. This simplification allows use of data from the Post Accident Heat Removal and fuel melt experiments performed for the LMFBR¹⁰ to derive a debris bed packing model for SCDAP. Measurements of fuel porosity, based on radiographs of a fuel particle bed that was heated to sodium boiling and then cooled, provided the following correlation for packed bed porosity, e...

$$\epsilon_{u} = 0.593 - 1.23 \times 10^{-4} B_{r}$$

where

 $B_F = debris bed loading per unit area (kg/m²).$

The value of $B_{\rm p}$ is calculated with the expression

$$B_{F} = \frac{M_{U}O_{2} + M_{Z}O_{2} + M_{Z}r + M_{S}t + M_{Ab}}{A_{r}}$$
(7)

(v)

where

It is noted that Equation (6) is valid for sodium coolant and bed loadings from 0 to 1000 kg/m². For water-UO₂, water-steel, water-lead, and

aceton-steel systems, correlation between bed porosity and bed loading for particle packing can not be derived due to the scatter of experimental data. 10

Since a rubble debris bed consists of loosely bound particles, the fragments may settle on the available horizontal space as a packed bed or be suspended in the upwardly flowing coolant as a fluidized bed, depending on the coolant flow rate. Furthermore, the debris particles may move out of the rubble debris region if the coolant velocity exceeds the terminal velocity of the particles.

For the packed bed configuration, the rubble debris bed pressure drop is calculated in the same manner as for the cohesive debris bed [Equation (3)]:

(8)

$$\frac{\Delta P_r}{u_0 H_r} = \alpha_r \mu + \beta_r G$$

where

a

Dr

 ΔP_r = coolant pressure drop across packed bed (Pa)

H = height of packed bed (m)

$$= 150 \frac{(1-\epsilon_r)^2}{\epsilon_r^3} \frac{1}{D_r^2}$$

$$\beta_r = 1.75 \frac{1-\epsilon_r}{\epsilon_r^3} \frac{1}{D_r}$$

= average particle diameter (m) [input from debris transition and propagation models]. As was the case for a cohesive debris bed, a characteristic length of the pore structure in a rubble debris bed can be calculated as

$$l_r = \frac{\beta_r}{\alpha_r} \quad . \tag{9}$$

The frictional pressure loss (ΔP_r) in a packed bed of solid particles increases as the superficial velocity of the coolant flowing upwardly through the bed increases. When the fluid velocity reaches a value that induces an upward drag on the particles equal to the weight of the particles, the bed becomes weightless. This condition is defined to be minimum or incipient fluidization. Any further increase in the fluid velocity produces an upward motion of the particles.

The minimum fluidization velocity can be calculated by setting pressure drop equal to debris bed weight per unit cross-sectional area and solving for velocity, as was done in Reference 13. This yields

$$u_f = 9.2975 \times 10^{-3} D_r^{1.82} \frac{\rho_f^{-0.06} (\rho_s - \rho_f)^{0.94}}{\mu^{0.88}}$$
 (10)

where

 P_s = density of debris bed material (kg/m³)

 P_{f} = density of fluid (kg/m³).

The density of the debris bed is calculated using the expression

$$P_{s} = \frac{M_{UO_{2}} + M_{ZrO_{2}} + M_{Zr} + M_{St} + M_{Ab}}{\frac{M_{UO_{2}}}{P_{UO_{2}}} + \frac{M_{ZrO_{2}}}{P_{ZrO_{2}}} + \frac{M_{Zr}}{P_{Zr}} + \frac{M_{St}}{P_{St}} + \frac{M_{Ab}}{P_{Ab}}}.$$
(11)

The data which support the correlation given by Equation (10) cover a wide range of particle size, particle diameter, and coolant density, as reported in Reference (5). The correlation is valid only for Reynolds numbers^a less than 7.57, and a correction factor is required for Reynolds numbers greater than 7.57. The correlation factor C_f is⁴

 $C_{f} = 1, \qquad \text{for } \text{Re} < 7.57$ $C_{f} = 1.364 - 0.18 \ln(\text{Re}), \qquad \text{for } 7.57 \leq \text{Re} < 200 \qquad \odot$ $C_{f} = 0.214 + 39.4/\text{Re}, \qquad \text{for } 200 \leq \text{Re} < 1000 \qquad (12)$ $C_{f} = 0.254, \qquad \text{for } \text{Re} \geq 1000.$

Using Equations (10) and (12), the minimum fluidization velocity, $\boldsymbol{u}_{\rm mf},$ can be expressed as

 $u_{mf} = C_f \cdot u_f$ (13)

This velocity is used to determine whether the debris particles will be in a packed bed configuration or in a fluidized state.

For a fluidized bed, the pressure drop across the bed remains constant with increasing flow _:e; i.e.,

 $\Delta P_{f} = H_{o} (\rho_{s} - \rho_{f}) g$ (14) where

 ΔP_f = coolant pressure drop across fluidized rubble bed (Pa)

a. Reynolds number is defined as GD_r/μ .

zero-porosity debris bed height (m)

$$= \left(\frac{{}^{M}_{U}U_{2}}{{}^{\rho}_{U}U_{2}} + \frac{{}^{M}_{Z}rU_{2}}{{}^{\rho}_{Z}rU_{2}} + \frac{{}^{M}_{Z}r}{{}^{\rho}_{Z}r} + \frac{{}^{M}_{St}}{{}^{\rho}_{St}} + \frac{{}^{M}_{Ab}}{{}^{\rho}_{Ab}}\right)\frac{1}{{}^{A}_{r}}$$

= gravitational acceleration constant (m/s²)

= 9.8.

Porosity of a fluidized bed is calculated as 14

$$\epsilon_{f} = \left(\frac{Re}{Re_{mf}} \cdot \epsilon_{mf}^{n}\right)^{\frac{1}{n}}$$
(15)

where

Ho

g

- \$ f = porosity of fluidized bed
 Re = Reynolds number of fluid flowing through fluidized bed
 Remf = Reynolds number of fluid at minimum fluidization velocity
 \$ mf = debris bed porosity at minimum fluidization velocity (Set
 - equal to ε_r based on the assumption that bed expansion will not occur before the pressure drop has reached the buoyant weight per unit area of bed).

In logarithmic coordinates, n is the slope of the line which represents the relationship between Reynolds number and fluidized bed porosity. According to the analysis of Richardson and Zaki, 14

n = 5.0, for Re < 0.2

12

$$n = \left(4.35 + 17.5 \frac{D}{D_{t}}\right) \operatorname{Re}^{-0.03}, \quad \text{for } 0.2 \le \operatorname{Re} < 1$$

$$n = \left(4.45 + 18 \frac{D_{r}}{D_{t}}\right) \operatorname{Re}^{-0.1}, \quad \text{for } 1 \le \operatorname{Re} < 200$$

$$n = 4.45 \operatorname{Re}^{-0.1}, \quad \text{for } 200 \le \operatorname{Re} < 500$$

$$n = 2.39, \quad \text{for } \operatorname{Re} \ge 500 \quad (16)$$

where

D_t = diameter of the debris bed (m) [input variable].

The fluidized bed height, L_{f} , is then calculated as

$$L_{f} = \frac{H_{0}}{1 - \varepsilon_{f}} \quad . \tag{17}$$

The height, H_{rd} , of the rubble debris region is specified by the debris transition and propagation models in SCDAP. To prevent the fluidized bed height from exceeding H_{rd} , L_f and ϵ_f are adjusted as follows if L_f is calculated to be greater than H_{rd} :

$$L_{f} = H_{rd}$$

$$\epsilon_{f} = 1 - \frac{H_{o}}{H_{rd}}$$
(18)

2.2 Debris Bed and Coolant Thermal Models

Debris bed and coolant temperatures are determined by simultaneous solution of the following two differential equations: $^{15}\,$

$$(1 - \varepsilon) \rho_p c_p \frac{\partial T_p}{\partial t} = (1 - \varepsilon) k_p \frac{\partial^2 T_p}{\partial z^2} - hv (T_p - T_c) + Q''' (1 - \varepsilon)$$

$$\epsilon \rho_{c} c_{c} \frac{\partial T_{c}}{\partial t} = \epsilon k_{c} \frac{\partial^{2} T_{c}}{\partial z^{2}} + hv (T_{p} - T_{c}) - G \epsilon c_{c} \frac{\partial T_{c}}{\partial z}$$
(19)

where

ε	=	debris bed porosity
°p'°c	=	density of debris bed and coolant (kg/m^3)
^c p, ^c c	=	specific heat of debris bed and coolant $(J/kg \cdot K)$
^k p, ^k c	-	thermal conductivity of debris bed and coolant $({\tt W/m{\mathchar}})$
т _р , т _с	=	debris bed and coolant temperature (K)
hv	=	volumetric heat transfar coefficient (W/m ³ •K)
Q'''	=	volumetric heat generation rate (W/m^3)
z	-	axial coordinate (m).

Before solving Equation (19), local coolant conditions and regions of analysis, heat generation, heat transfer coefficient between solid and coolant, and debris bed dryout analysis will be discussed. These discussions will be followed by a description of the temperature solution and propagation of a melt front within a debris bed.

2.2.1 Local Coolant Condition and Regions of Analysis

A debris bed can be divided into the following three regions based on the coolant temperature distribution in the ped:

 Subcooled region where coolant temperature is less than the coolant saturation temperature at the system pressure

- Saturated region where coolant temperature is equal to the coolant saturation temperature
- 3. Superheated region where coolant temperature is greater than the coolant saturation temperature.

Here, coolant temperature is considered to represent the homogeneous temperature of the coolant with the assumption of perfect mixing of the liquid and vapor phases.

For a given coolant flow rate and debris bed volumetric heat generation rate, the height of the subcooled, saturated, and superheated regions can be calculated as follows:

$$L_{sc} = \frac{\rho_c V_c c_c}{Q'(1 - \epsilon)} (T_{sat} - T_{in})$$

$$L_{sa} = \frac{\rho_c V_c h_{fg}}{Q'(1-\varepsilon)}$$

where

sc	=	subcooled region height (m)
sa	8	saturated region heignt (m)
sp		superheated region height (m)
V	=	coolant velocity (m/s)

(20)

T_{sat} = coolant saturation temperature at system pressure (K)

T_{in} = coolant inlet temperature (K)

 h_{fo} = latent heat of evaporation (J/kg)

H_d = debris bed height (m).

Figure 1 shows the possible combinations of regions for the temperature analysis. Also shown in the figure is the assigned debris identification number, IDREGN, for the different possible configurations. For each subcooled and superheated region, the region is divided into nd equally spaced nodes for the temperature analysis. For the saturated region, all of the heat generated within the bed is assumed to be consumed in evaporating saturated coolant (raising quality from 0 to 1). Coolant temperature remains at the saturation temperature, and the bed temperature remains the same as the previous nodal temperature. Thus, only three nodes are used for specifying the temperature of the coolant and debris bed in a saturated region. Based on the above discussion and with reference to Figure 1, the total number of nodes, NOND, is

1	nd,	for	IDREGN	=	1
가슴만	nd,	for	IDREGN	=	2
NOND =	3,	for	IDREGN	=	3
	nd + 2,	for	IDREGN	=	4
	nd + 2,	for	IDREGN	=	5
	2nd + 1,	for	IDREGN	=	6

(21)

During the calculation of debris bed and coolant temperatures, heights of the different regions may change and/or different regions may be used due to changes in heat generation rate, coolant flow rate, etc. A model (REGMOD) has been developed to redefine the total number of nodes, node elevations, and coolant and debris bed temperatures corresponding to each



Figure 1. Possible regions to be analyzed in a debris bed.

node. The temperatures for each node are determined by REGMOD using interpolation of the previous nodal temperatures.

2.2.2 Heat Generation

The primary sources of heat generation within a debris bed will be decay heat (and possible fission heat for in-pile experiments) and chemical heat of reaction associated with Zircaloy oxidation at elevated temperatures. The heat source included in Equation (19) includes the above such heat sources. However, the magnitude of heat generation due to the different possible sources is an input to the debris characterization and behavior models described herein. Because decay heat and oxidation heat can be sensitive to the debris bed temperature, the heat source used in Equation (19) may need to reflect the bed temperature. The debris bed thermal models include an iteration scheme which can be used to obtain a consistant heat source and temperature solution.

2.2.3 Heat Transfer Coefficient

Because of the difficulties associated with assigning a heat-transfer surface area and temperature difference between the solid and fluid in a debris bed, the heat transfer coefficient between debris bed and coolant which appears in Equation (19) is based on the volume of the porous system. Using the characteristic length of the pore structure (1_c or 1_r), the Nusselt and Reynold's numbers are defined as¹⁶

$$Nu = \frac{hv1^2}{k_c}$$

 $Re = \frac{G1}{\mu}$

10

(22)

where 1 equals l_c or l_r for a cohesive bed and rubble bed, respectively.

In the subcooled and saturated regions of either a cohesive debris bed or packed bed, hv is given as $^{17}\,$

$$hv = \left[(7 - 10\epsilon + 5\epsilon^{2})(1 + 0.7 \text{ Re}^{0.3} \text{Pr}^{\frac{1}{3}}) + (1.33 - 2.4\epsilon + 1.2\epsilon^{2}) \right]$$

$$Re^{0.7} \text{Pr}^{\frac{1}{3}} \frac{k_{c}}{1^{2}}$$
(23)

where

Pr = Prandtl number

=

 $\epsilon = \epsilon_c \text{ or } \epsilon_r$ for cohesive and rubble bed, respectively.

In the subcooled region of a fluidized rubble debris bed, hv is expressed as $^{18}\,$

hv = 1.28 x 10⁵ (Re Fe)² Pr^{0.67}
$$(\frac{\mu}{\mu_R})^{0.83} \left(\frac{D_t}{D_r}\right) \left(\frac{\rho_s}{\rho_c}\right)^2 \left(\frac{k_c}{1_r^2}\right)$$
 (24)

where

$$Fe = [1 - 1.209(1 - e_f)^{2/3}]^{-1}$$

 μ_R = coolant viscosity for water at 300 K.

For a saturated region of a fluidized rubble bed, hv is correlated as 19

$$hv = 2.2 \times 10^{5} \text{ pr}^{-2.13} \left[\left(\frac{T_{\text{sat}}^{c}}{h_{\text{fg}}} \right) \left(\frac{\mu_{1}^{2} F \epsilon^{2}}{h_{\text{fg}}^{2} v^{g}} \right) \right]^{0.84} \left[\frac{D_{r}^{2} (\rho_{f} - \rho_{v})}{\sigma_{g}} \right]^{0.5} \frac{k_{1}}{1_{r}^{2}}$$
(25)

where

σ

= surface tension of coolant (kg/s²)

59.3 for water at 373 K

 $\rho_1, \rho_v = \text{density of liquid and vapor phases, respectively} (kg/m³).$

=

In a superheated region for either a cohesive or rubble debris bed, 20

$$hv = \left[\frac{1}{0.00377}\right]^{1.33} \frac{Re^{0.65}k_c}{1^2} .$$
 (26)

2.2.4 Debris Bed Dryout

For a debris bed immersed in a pool of fluid with an insulated bottom or with a forced flow of fluid through the bottom of the bed, debris bed dryout is defined to occur when the vapor generation rate is sufficiently large to preclude an adequate flow of replenishing liquid. Such a situation might lead to a sustained temperature rise within the bed and subsequent melting of the debris bed material. Research on dryout in a rubble bed has been conducted by several experimenters^{12,21-30} and has involved water, acetone, methanol, and sodium with steel, lead, sand, and urania. Of the several dryout models available in the literature, the model developed by Lipinski (References 28-30) is one of the most recent. In addition, Lipinski's model considers bottom flooding in deep beds, as may occur in an LWR severe accident sequence. A model (DRYOUT) has been developed based on Lipinski's research. The model is described below.

Through algebraic manipulation of the one-dimensional conservation equations for two-phase, counter-current flow in a porous medium, Lipinski developed a simple quadratic equation for the debris bed heat flux (q) as a function of the effective saturation in the bed (Se). The equation is

$$\frac{1.75 (1 - \epsilon)}{d\epsilon^{3} h_{fg}^{2}} \left[\frac{1}{\rho_{v}(1 - Se)^{3}} \pm \frac{1}{\rho_{1}Se^{3}} \right] q^{2} + \left[\frac{180 (1 - \epsilon)^{2}}{d^{2}\epsilon^{3} h_{fg}} \left(\frac{\mu_{v}}{\rho_{v}(1 - Se)^{3}} + \frac{1}{\rho_{1}Se^{3}} \right) + \frac{3.5 (1 - \epsilon) G}{d\epsilon^{3} \rho_{1}Se^{3} h_{fg}} \right] q \pm \frac{1.75 (1 - \epsilon) G^{2}}{d\epsilon^{3} \rho_{1}Se^{3}} - \frac{180 (1 - \epsilon)^{2} \mu_{1}G}{d^{2}\epsilon^{3} \rho_{1}Se^{3}} - \frac{160 (1 - \epsilon)^{2} \mu_{1}G}{d^{2}\epsilon^{3} \rho_{1}Se^{3}} - \frac{160 (1 - \epsilon)^{2} \mu_{1}G}{d^{2}\epsilon^{3} \rho_{1}Se^{3}} + \frac{1}{2} \left(\frac{1}{2} \frac{1}{2}$$

where

ε	=	debris bed porosity
d	=	debris particle diameter (m)
°v, °l	=	density of vapor and liquid phase of coolant $({\rm kg/m}^3)$
q	-	debris bed heat flux (W/m ²)

bed effective saturation

Se

 $\mu_{v}, \mu_{1} = viscosity of vapor and liquid phases of coolant <math>(kg/m^{2} \cdot s).$

For $q > Gh_{fg}$, the upper arithmetic operation in Equation (27) is used. For $q < Gh_{fg}$, the lower arithmetic operation is used.

Heat fluxes predicted with Equation (27) are shown in Figure 2. The dryout heat flux is given by the maximas in the curves of heat flux versus the effective saturation of the bed. As the flow of liquid into the bottom of the bed increases, the maximum point on the heat flux versus effective saturation curves approaches an effective saturation of zero. Physically, this implies that the dryout heat flux (q_d) becomes equal to the heat required to vaporize all of the liquid entering the bottom of the bed ($q_d = Gh_{fg}$) and that the penetration of liquid from the top is precluded.

As discussed in Reference (31), the factors significant in calculating dryout heat flux are coolant properties and bed characteristics such as bed void fraction and particle diameter. As shown in Figure 3 (Figure 3 of Reference 31), dryout heat flux increases with bed void fraction and particle size for low or zero bottom flow rates. When the bottom flow rates become large enough that the effective saturation becomes zero at dryout, dryout heat fluxes become independent of bed void fraction and particle size.

The DRYOUT model numerically solves for the maximum hest flux (the dryout heat flux) predicted by Equation (27) given values of the dependent variables which describe the state of the debris bed. The calculated dryout heat flux is then compared with the local heat flux. If the local heat flux is greater than the dryout heat flux, the heat transfer coefficient given by Equation (26) is used in the subsequent temperature calculations. If not, the heat transfer coefficient as calculated with Equations (23), (24), or (25) is used in the temperature calculations.

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Figure 2. Dryout heat flux from Equation (27).



Figure 3. Dryout heat flux dependency upon coolant mass flux, bed void fraction, and particle size.

2.2.5 Temperature Solution

In the subcooled and superheated regions of a debris bed, nd equallyspaced nodes are used to solve Equation (19). The finite difference form of Equation (19) is:

$$P_{pn} c_{pn} \frac{T_{pn}^{m+1} - T_{pn}^{m}}{\Delta t} = \frac{k_{pn,n+1} \left(T_{pn+1}^{m+1/2} - T_{pn}^{m+1/2}\right) - k_{pn-1,n} \left(T_{pn}^{m+1/2} - T_{pn-1}^{m+1/2}\right)}{\Delta z^{2}}$$
$$- \frac{hv}{1 - \varepsilon} \left(T_{pn}^{m+1/2} - T_{cn}^{m+1/2}\right) + Q^{'''}$$
$$P_{cn} c_{cn} \frac{T_{cn}^{m+1} - T_{cn}^{m}}{\Delta t} = \frac{k_{cn,n+1} \left(T_{cn+1}^{m+1/2} - T_{cn}^{m+1/2}\right) - k_{cn-1,n} \left(T_{cn}^{m+1/2} - T_{cn-1}^{m+1/2}\right)}{\Delta z^{2}}$$

$$+ \frac{hv}{\epsilon} \left(T_{pn}^{m+1/2} - T_{cn}^{m+1/2} \right) - Gc_{cn} \frac{T_{cn+1}^{m+1/2} - T_{cn-1}^{m+1/2}}{2\Delta z}$$
(28)

where

$$T_{pn}^{m+1/2}, T_{cn}^{m+1/2} = 1/2 \left(T_{pn}^{m+1} + T_{pn}^{m} \right) \text{ and } 1/2 \left(T_{cn}^{m+1} + T_{cn}^{m} \right),$$
respectively (K)
$$\Delta z = \text{space between spatial nodes (m)}$$

$$\Delta t = \text{time step (s).}$$

The implicit finite difference form of Equation (28) with the appropriate boundary conditions is given below.

For the debris,

n=1

$$T_{p2}^{m+1}\left(-\frac{k_{p1,2}}{\Delta z^{2}}\right)+T_{p1}^{m+1}\left[\frac{\rho_{p1}c_{p1}}{\Delta t}+\frac{k_{p1,2}}{\Delta z^{2}}+\frac{hv}{2(1-\varepsilon)}\right]+T_{c1}^{m+1}\left[-\frac{hv}{2(1-\varepsilon)}\right]$$
$$=T_{p2}^{m}\left(-\frac{k_{p1,2}}{\Delta z^{2}}\right)+T_{p1}^{m}\left[\frac{\rho_{p1}c_{p1}}{\Delta t}+\frac{k_{p1,2}}{\Delta z^{2}}+\frac{hv}{2(1-\varepsilon)}\right]+T_{c1}^{m}\left[-\frac{hv}{2(1-\varepsilon)}\right]$$
$$+Q^{'''}+2\cdotHTLBCD/\Delta z$$
(29)

n=n

$$T_{pn+1}^{m+1}\left(-\frac{k_{pn,n+1}}{2\Delta z^{2}}\right) + T_{pn}^{m+1}\left[\frac{\rho_{pn}c_{pn}}{\Delta t} + \frac{k_{pn,n+1}}{2\Delta z^{2}} + \frac{k_{pn-1,n}}{2\Delta z^{2}} + \frac{hv}{2(1-\varepsilon)}\right] + T_{pn-1}^{m+1}\left(-\frac{k_{pn-1,n}}{2\Delta z^{2}}\right) + T_{pn}^{m+1}\left(-\frac{k_{pn,n+1}}{2\Delta z^{2}}\right) + T_{pn}^{m}\left[\frac{\rho_{pn}c_{pn}}{\Delta t} + \frac{k_{pn,n+1}}{2\Delta z^{2}} + \frac{k_{pn,n+1}}{2\Delta z^{2}}\right] + \frac{k_{pn-1,n}}{2\Delta z^{2}}\right] + \frac{k_{pn-1,n}}{2\Delta z^{2}} + \frac{k_{pn-1,n}}{2\Delta z^{2}} + \frac{k_{pn-1,n}}{2\Delta z^{2}} + \frac{k_{pn-1,n}}{2\Delta z^{2}}\right) + T_{pn}^{m}\left[\frac{\rho_{pn}c_{pn}}{\Delta t} + \frac{k_{pn,n+1}}{2\Delta z^{2}}\right] + Q^{'''} (30)$$

$$T_{pN}^{m+1} \left[\frac{P_{pN}C_{pN}}{\Delta t} + \frac{k_{pN-1,N}}{\Delta z^{2}} + \frac{hv}{2(1-\varepsilon)} \right] + T_{pN-1}^{m+1} \left(-\frac{k_{pN-1,N}}{\Delta z^{2}} \right) + T_{cN}^{m+1} \left[-\frac{hv}{2(1-\varepsilon)} \right]$$

$$= T_{pN}^{m} \left[\frac{P_{pN}C_{pN}}{\Delta t} + \frac{k_{pN-1,N}}{\Delta z^{2}} + \frac{hv}{2(1-\varepsilon)} \right] + T_{pN-1}^{m} \left(-\frac{k_{pN-1,N}}{\Delta z^{2}} \right) + T_{cN}^{m} \left[-\frac{hv}{2(1-\varepsilon)} \right]$$

$$+ q^{'''} + \frac{2 \cdot \text{HTUBCD}}{\Delta z}$$
(31)

For the coolant,

$$T_{c2}^{m+1} \left(-\frac{k_{c1,2}}{\Delta z^{2}} + \frac{Gc_{c1}}{2\Delta z} \right) + T_{c1}^{m+1} \left(\frac{\rho_{c1}c_{c1}}{\Delta t} + \frac{k_{c1,2}}{\Delta z^{2}} + \frac{hv}{2\varepsilon} - \frac{Gc_{c1}}{2\Delta z} \right) + T_{p1}^{m+1} \left(-\frac{hv}{2\varepsilon} \right)$$

$$= T_{c2}^{m} \left(-\frac{k_{c1,2}}{\Delta z^{2}} + \frac{Gc_{c1}}{2\Delta z} \right) + T_{c1}^{m} \left(\frac{\rho_{c1}c_{c1}}{\Delta t} + \frac{k_{c1,2}}{\Delta z^{2}} + \frac{hv}{2\varepsilon} - \frac{Gc_{c1}}{2\Delta z} \right)$$

$$+ T_{p1}^{m} \left(-\frac{hv}{2\varepsilon} \right) + \frac{2 \cdot HTLBCC}{\Delta z}$$

$$(32)$$

n=n

$$T_{cn+1}^{m+1} \left(-\frac{k_{cn,n+1}}{2\Delta z^{2}} + \frac{Gc_{cn}}{4\Delta z} \right) + T_{cn}^{m+1} \left(\frac{p_{cn}c_{cn}}{\Delta t} + \frac{k_{cn,n+1}}{2\Delta z^{2}} + \frac{k_{cn-1,n}}{2\Delta z^{2}} + \frac{hv}{2\varepsilon} \right) + T_{cn-1}^{m+1} \left(-\frac{k_{cn,n+1}}{2\Delta z^{2}} - \frac{Gc_{cn}}{4\Delta z} \right) + T_{pn}^{m+1} \left(-\frac{hv}{2\varepsilon} \right) = T_{cn+1}^{m} \left(-\frac{k_{cn,n+1}}{2\Delta z^{2}} + \frac{Gc_{cn}}{2\Delta z^{2}} + \frac{Gc_{cn}}{2\Delta z^{2}} + \frac{Gc_{cn}}{2\Delta z^{2}} + \frac{Gc_{cn}}{2\Delta z^{2}} + \frac{F_{cn-1,n}}{2\Delta z^{2}} + \frac{F_{cn-1,n}}{2\Sigma} + \frac{F_{cn-1,n}}{2\Sigma}$$

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+
$$T_{cn-1}^{m}\left(-\frac{k_{cn-1,n}}{2\Delta z^{2}}-\frac{Gc_{cn}}{4\Delta z}\right)$$
+ $T_{pn}^{m}\left(-\frac{hv}{2\varepsilon}\right)$ (33)

n=nd=N

$$T_{CN}^{m+1} \left(\frac{P_{CN}C_{CN}}{\Delta t} + \frac{k_{CN-1,N}}{\Delta z^2} + \frac{hv}{2\varepsilon} + \frac{GC_{CN}}{2\Delta z} \right) + T_{CN-1}^{m+1} \left(-\frac{k_{CN-1,N}}{\Delta z^2} - \frac{GC_{CN}}{2\Delta z} \right) + T_{pN}^{m+1} \left(-\frac{hv}{2\varepsilon} \right) = T_{CN}^m \left(\frac{P_{CN}C_{CN}}{\Delta t} + \frac{k_{CN-1,N}}{\Delta z^2} + \frac{hv}{2\varepsilon} + \frac{GC_{CN}}{2\Delta z} \right) + T_{CN-1}^m \left(-\frac{k_{CN-1,N}}{\Delta z^2} - \frac{GC_{CN}}{2\Delta z} \right) + T_{CN-1}^m \left(-\frac{k_{CN-1,N}}{\Delta z^2} - \frac{GC_{CN}}{2\Delta z} \right) + T_{pN}^m \left(-\frac{hv}{2\varepsilon} \right) + \frac{2 \cdot HTUBCC}{\Delta z}$$
(34)

where

$$HTLBCD = heat transfer into debris bed at lower boundary (W/m2)$$

$$HTLBCC = heat transfer into coolant at lower boundary (W/m2)$$

$$HTUBCD = heat transfer into debris bed at upper boundary (W/m2)$$

$$HTUBCC = heat transfer into coolant at upper boundary (W/m2).$$

The matrix form of Equations (29) through (34) is

$$\begin{bmatrix} A_{11} & A_{12} \\ A_{21} & A_{22} \end{bmatrix} \cdot T = R$$
(35)

where




$$\begin{bmatrix} \frac{P_{c1}^{c}c_{c1}}{\Delta t} + \frac{k_{c1,2}^{2}}{\Delta z^{2}} + \frac{h_{v}}{2\epsilon} - \frac{6c_{c1}}{2\Delta z} \end{bmatrix} \begin{bmatrix} \frac{k_{c1,2}}{\Delta z^{2}} + \frac{6c_{c1}}{2\Delta z} \end{bmatrix}$$

$$\begin{bmatrix} \frac{k_{c1,2}}{2\Delta z^{2}} - \frac{6c_{c2}}{4\Delta z} \end{bmatrix}$$

$$\begin{bmatrix} \frac{k_{c1,2}}{2\Delta z^{2}} - \frac{6c_{c2}}{4\Delta z} \end{bmatrix}$$

$$\begin{bmatrix} \frac{k_{c1,2}}{2\Delta z^{2}} - \frac{6c_{c1}}{4\Delta z} \end{bmatrix}$$

$$\begin{bmatrix} \frac{k_{c1,2}}{2\Delta z^{2}} + \frac{6c_{c1,2}}{4\Delta z} \end{bmatrix}$$

$$\begin{bmatrix} \frac{k_{c1,2}}{2\Delta z^{2}} + \frac{6c_{c1,2}}{4\Delta z} \end{bmatrix}$$

A₂₂ =



The large circles in matrices A_{11} , A_{12} , A_{21} , and A_{22} signify that the off-diagonal or off-tridiagonal elements are zero. Thus, there are 2N linear equations, the first N equations for the debris temperatures and the remaining N equations for the coolant temperatures. The equations are solved simultaneously.

The TEMPSR model solves the above matrix of equations to obtain the debris bed and coolant temperatures. For a saturated region, the coolant temperature is assumed to equal the saturation coolant temperature. The debris temperature is equal to the previous nodal temperature. Thus, calculations of coolant and debris bed temperatures are not needed for the saturation region.

2.2.6 Melting Front Propagation

The debris bed thermal models employ a simplified approach for describing propagation of a melt front within a debris bed. The following assumptions are used:

- 1. Axial heat conduction is infinite.
- Super heating of the molten material does not occur until all of the debris bed has melted.

If the calculated debris bed temperature T_i at node i is greater than the melting temperature of the debris bed material, T_{mt} , the bed temperature at node i is set equal to the value of T_{mt} . The energy excess, $p[c_p(T_i - T_{mt}) - h_{sf}]\Delta V_i$, is assumed to increase the temperature of the debris material at node i-1. (ρ , c_p , h_{sf} , and ΔV_i are debris bed density, debris bed specific heat, latent heat of fusion for debris material, and debris bed volume associated with node i, respectively.) The debris material at node i-1 is first heated to the melting temperature. If the energy excess from node i is large enough, the debris material at node i-1 may be melted and the process may progress downward to node i-2, etc. Propagation of a melt front, as described above, is analyzed by the FRAGTH and FROZTH models for the rubble and cohesive debris beds, respectively. Based on the progression of the melt front during any time step, the FRMELT and FGMELT models calculate the velocity of the front in the rubble and debris beds, respectively. Based on this velocity, the FRESTT and FGESTT models estimate the time when the melt front will reach the lower boundary of the rubble and cohesive debris beds, respectively.

2.3 Applicability Range of Correlations

Many of the equations described in Sections 2.1 and 2.2 have been derived empirically. Table 1 summarizes the data ranges of these empirical correlations. Also shown are the expected ranges of application of the correlations for SCDAP. For the most part, the ranges of the correlations span the expected range of application for SCDAP analyses. Planned assessment of SCDAP will demonstrate if exceeding the data ranges of the correlations is significant. Experimental data on debris bed behavior for LWR conditions will be obtained during the next several years. This data will provide a basis for removing deficiencies which exist in the present modeling.

Data Range	Expected Application Range
$\begin{array}{l} 0.3 < \varepsilon < 0.8 \\ 0.2 < Re < 3500 \\ 1.5 \times 10^{-4} < D_{\rm D}({\rm m}) < 2 \times 10^{-3} \end{array}$	$0.2 < \epsilon < 1$ $0 < Re < 1.2 \times 10^5$ $1.9 \times 10^{-5} < D_p(m) < 3 \times 10^{-3}$
$0 < B_{\rm F}(kg/m^2) < 1000$	$0 < B_F (kg/m^2) < 3.5 \times 10^4$
$0.3 < \epsilon < 0.8$	$0.2 < \epsilon < 1$
$0.001 < Re < 10^{6}$	$0 < \text{Re} < 1.2 \times 10^5$
$5.1 \times 10^{-5} < 0_{p}(m) < 5.2 \times 10^{-3}$	$1.9 \times 10^{-5} < 0_p(\text{m}) < 3 \times 10^{-3}$
0.02 < Re < 1000	$0 < \text{Re} < 1.2 \times 10^5$
$0 < \text{Re}^{3} < 10^{2}$	$0 < Re^{2} < 1.0 \times 10^{2}$
0.35 < c < 1.0	$0.2 < \epsilon < 1$
1.0 x 10^{-1} < Re ^a < 2.0 x 10^{2}	$0 < \text{Re}^3 < 1.0 \times 10^2$
1.6 x 10^{-3} < $D_r(m)$ < 4.8 x 10^{-3}	1.9 x 10 ⁻⁵ < 0 _r (m) < 3 x 10 ⁻³
0.611 < ϵ < 0.862	0.2 < ϵ < 1
$0.6 < \epsilon < 1$	$0.2 < \epsilon < 1$
1.1 x $10^{-2} < \text{Re}^3 < 1.7 x 10^{-1}$	$0 < Re^{a} < 1.0 \times 10^{2}$
$2 \times 10^{-4} < d(m) < 2 \times 10^{-2}$	1.9 x $10^{-5} < d(m) < 3 x 10^{-3}$
$0 < \epsilon < 1$	0.2 < $\epsilon < 1$
0 < Se < 1	0 < Se < 1
	$\begin{array}{c} \text{Data Range} \\ \hline 0.3 < \varepsilon < 0.8 \\ 0.2 < \text{Re} < 3500 \\ 1.5 \times 10^{-4} < 0_p(\text{m}) < 2 \times 10^{-3} \\ 0 < B_F(\text{kg/m}^2) < 1000 \\ \hline 0.3 < \varepsilon < 0.8 \\ 0.001 < \text{Rg} < 106 \\ 5.1 \times 10^{-5} < 0_p(\text{m}) < 5.2 \times 10^{-3} \\ 0.02 < \text{Re} < 1000 \\ \hline 0 < \text{Re}^3 < 10^2 \\ 0.35 < \varepsilon < 1.0 \\ \hline 1.0 \times 10^{-1} < \text{Re}^3 < 2.0 \times 10^2 \\ 1.6 \times 10^{-3} < 0_F(\text{m}) < 4.8 \times 10^{-3} \\ 0.611 < \varepsilon < 0.862 \\ \hline 0.6 < \varepsilon < 1 \\ 1.1 \times 10^{-2} < \text{Re}^3 < 1.7 \times 10^{-1} \\ 2 \times 10^{-4} < d(\text{m}) < 2 \times 10^{-2} \\ 0 < \text{Se} < 1 \\ \hline 0 < \text{Se} < 1 \\ \hline \end{array}$

TABLE 1. SUMMARY OF DATA RANGES AND EXPECTED RANGES FOR CORRELATIONS IN SECTION 2

a. Reynolds number is defined in Equation (22).

3. DESCRIPTION AND IMPLEMENTATION OF COMPUTER MODELS

3.1 Implementation in SCDAP

The debris bed characterization and thermal behavior models described in this report will be employed by the DBUNDL subroutine in SCDAP. DBUNDL controls analysis of a disrupted fuel bundle. The functional decomposition of DBUNDL, shown in Table 2, illustrates the relationship of the subroutines (models) which are used to perform analysis of a disrupted bundle. The models described in Section 2 are contained in the subroutines DBFRGZ and DBFRAG and the subroutines accessed by these subroutines. Subroutines DBFROZ and DBFRAG serve as the driver programs which direct the logic flow for the debris behavior models associated with the cohesive and rubble beds, respectively. The hierarchy of the subroutines called by DBFROZ and DBFRAG is shown in Tables 3 and 4, respectively. As shown by Tables 3 and 4, several of the subroutines are common to both DBFROZ and DBFRAG.

A driver program, DBDRIV, was developed to test DBFROZ and DBFRAG. In addition to calling DBFROZ and DBFRAG, the driver calls three other subroutines: DEBINP, DBTIME, and DBOUTD. The general purposes of DBTIME and DBOUTD are described in Table 2. The purpose of DEBINP is to provide input for DBFROZ and DBFRAG by simulating output from DBTRAN and DBREGN. Although DEBINP, DBTIME, and DBOUTD are routines that form part of the SCDAP functional decomposition, these same routines which have been developed for the driver, DBDRIV, are only temporary. However, they are comparable to what will be used by SCDAP and help define the final requirements for the SCDAP routines.

3.2 Description of Computer Models

FORTRAN listings of the subroutines included in DBFROZ and DBFRAG are given in Appendix A of this report. Also, FORTRAN listings of the driver program, DBDRIV, and the subroutines DEBINP, DBTIME, and DBOUTD are

TABLE 2. DBUNDL FUNCTIONAL DECOMPOSITION

Subroutine	Function
DBUNDL	Disrupted bundle analysis
DBOUT	Disrupted bundle output
DBOUTD	Debris region output
DBTIME	Disrupted bundle time step
- DBANA	Disrupted bundle average behavior
- DBREGN	Region boundaries
DBTRAN	Region boundary conditions
- DBNTAC	Intact bundle region analysis
- DBFRAG	Rubble debris analysis
FGTIME	Rubble debris time step
- FGCHAR	Debris bed characteristics
FRAGTH	Debris thermally related behavior
FGMELT	Melting front propagation
FGESTT	Boundary disruption time estimation
LDBFROZ	Cohesive debris analysis
- FRTIME	Cohesive debris time step
FRCHAR	Debris bed characteristics
- FROZTH	Debris thermally related behavior
- FRMELT	Melting front propagation
FRESTT	Boundary disruption time estimation

TABLE 3. DESCRIPTION OF DBFROZ

Subroutine	Function
DBFROZ	
FRTIME	Determines time steps for cohesive debris bed analysis
-FRCHAR	Computes debris bed characteristics and debris hydraulic behavior
- FROZTH	Calculates debris bed and coolant temperatures and thermally-related behavior
DRYOUT	Computes dryout heat flux of debris bed
U SMNMX ^a	Finds largest value in a vector
REGMOD	Modifies region identification number and temperature distribution along debris bed
- ICSCCUª	
ICSEVU ^a	Interpolation subroutines
TEMPSR	Solves for debris bed and coolant temperature
- LSGECOA	Factors a real matrix by Gaussian elimination and estimates the condition of the matrix
L SGESL ^a	Solves the real system A*X=B
— СНЕМНТЬ	Computes Zr-steam reaction heat and H_{2} release
- NUCLHT ^b	Computes debris decay power
GASRLSD	Computes fission product release
- FRMELT	Calculates movement of melt front in cohesive debris bed
FRESTT	Estimates time when melt front will reach lower boundary of cohesive debris bed

a. Utility or library subroutine.

b. Currently inactive subroutine.

TABLE 4. DESCRIPTION OF DBFRAG

Subroutine	Function
DBFRAG	
-FGTIME	Determines time steps for rubble debris bed analysis
— F GCHAR	Computes debris bed characteristics and debris hydraulic behavior
FRAGTH	Calculates debris bed and coolant temperatures and thermally-related behavior
DRYOUT	Computes dryout heat flux of debris bed
USMNMXa	Finds largest value in a vector
REGMOD	Modifies region identification number and temperature distribution along debris bed
- ICSCCUª	
ICSEVUa	Interpolation subroutines
- TEMPSR	Solves for debris bed and coolant temperature
L SGECO ^a	Factors a real matrix by Gaussian elimination and estimates the condition of the matrix
L SGESL ^a	Solves the real system A*X=B
- СНЕМНТЬ	Computes Zr-steam reaction heat and H ₂ release
NUCLHT ^b	Computes debris decay power
GASRLSb	Computes fission product release
- FGMELT	Calculates movement of melt front in rubble debris bed
FGESTT	Estimates time when melt front will reach lower boundary of rubble debris bed

1

a. Utility or library subroutine.

b. Currently inactive subroutine.

given in Appendix A. The input and output variables for DBFROZ and DBFRAG and the subroutines called by DBFROZ and DBFRAG are listed in Tables 5 through 19.

TABLE 5. INPUT/OUTPUT DESCRIPTION FOR DBFROZ

USE	FORTRAN	SYMBOL	DESCRIPTION	UNIIS
INPUT	ABSMC	M _{Ab}	TOTAL MASS OF CONTROL ROD MATERIAL ACCUMULATED	КG
INPUT	ALPHAC	(1)	EFFECTIVE ALPHA-ZR REACTION AREA	M2
INPUT	ALPHTC	(1)	EFFECTIVE ALPHA-ZR REACTION LAYER THICKNESS	м
INPUT	AREAR	A _c	TOTAL BUNDLE CROSS SECTIONAL AREA IN DEBRIS	M2
INPUT	DELTT	Δt	TIME STEP	5
INPUT	ELVNC	(2)	ELEVATION OF POROUS BODY-FROM THE BOITOM OF ROD BUNDLE TO THE BOTTOM OF POROUS BODY REGION	M
INPUT	HITEC	Н	FROZEN DEBRIS REGION HEIGHT FROM DBREGN	۲
INPUT	HTLBCC	нтьвсс	HEAT TRANSFER INTO COHESIVE DEBRIS COOLANT AT	W/M2
INPUT	HTLBCD	HTLBCD	HEAT TRANSFER INTO COHESIVE DEBRIS BED TO LOWER BOUNDARY	W/M2
INPUT	нтивсс	HTUBCC	HEAT TRANSFER INTO COHESIVE DEBRIS CODLANT AT	W/M2
INPUT	HTUBCD	HTUBCD	HEAT TRANSFER INTO COHESIVE DEBRIS BED AT JPPER BOUNDARY	W/M2
INPUT	I	(2)	INDEX OF CURRENT TIME FROM TIME ARRAY	
INPUT	MAXL	(2)	MAXIMUM NUMBER OF NODES IN THE DEBRIS REGION WHICH COMBINED LIQUID, SATURATION, AND VAPOR REGION	
INPUT	ND	nd	NUMBER OF NODES TO BE USED IN LIQUID OR VAPOR REGION FOR DEBRIS REGION	
INPUT	NT	(2)	NUMBER OF TIME STEPS IN THE TIME ARRAY	

TABLE 5. (CONTINUED)

USE	FORTRAN	SYMBOL	DESCKIPTION	UNITS
INPUT	STRMC	M _{St}	TOTAL MASS OF CORE STRUCTURAL MATERIALS ACCUMULATED IN COMESIVE DEBRIS BED	KG
INPUT	т	(2)	TIME STEP ARRAY	5
INPUT	UO2MC	MUO2	TOTAL MASS OF UD2 ACCUMULATED FOR ALL COMPONENTS	КG
INPUT	VINC	u _o	COOLANT VELOCITY AT BOTTOM OF COHESIVE DERRIS REGION	M/5
INPUT	VINCOD	(2)	COOLANT VELOCITY AT BOTTOM OF COHESIVE DEBRIS REGION AT PREVIOUS TIME STEP	MIS
INPUT	XMASSC	(2)	TOTAL MASS OF DEBRIS ACCUMULATED FOR ALL COMPONENTS IN COHESIVE DEBRIS BED	КG
INPUT	ZRMC	MZr	TOTAL MASS OF ZR ACCUMULATED FOR ALL COMPONENTS	KG
INPUT	ZROZAC	(1)	EFFECTIVE ZR-STEAM REACTION AREA	M2
INPUT	ZRUZMC	MZr02	TOTAL MASS OF ZROZ ACCUMULATED FOR ALL COMPONENTS IN COHESIVE DEBRIS BED	КG
INPUT	ZROZTC	(1)	EFFECTIVE ZROZ REACTION LAYER THICKNESS	м
I/0	BEDTMP	Τ _ρ	DEBRIS BED TEMPERATURE CORRESPONDING TO AXIAL NODES	к
1/0	COLTMP	Т _с	DEBRIS BED COOLANT TEMPERATURE CORRESPONDING TO AXIAL NODES	ĸ
1/0	ELVAY	(2)	ELEVATION OF DEBRIS AXIAL NODES	м
1/0	FGRSC	(1)	FISSION GAS RELEASE DURING DELTT	MALES
1/0	FISHC	(1)	FISSION DECAY HEAT GENERATION RATE	W/M3
1/0	TOREGN	IDREGN	DEBRIS REGION ID NUMBER OF LAST TIME STEP	

TABLE 5. (CONTINUED)

USE	FORTRAN	SYMBOL	DESCRIPTION	UNITS
1/0	NOND	NOND	NUMBER OF TOTAL NODES IN THE ANALYSIS	
I/0	OXDAC	(1)	ZR-STEAM HEAT GENERATION RATE	W/M3
1/0	VOLGSC	(1)	VOLATILE FISSION PRODUCTS RELEASE FURING DELTT	MOLE
OUTPUT	CURTIM	(2)	CURRENT TIME	S
OUTPUT	DOWNZ	(2)	LENGTH OF MOLTEN POOL PENETRATION IN COHESIVE DEBRIS	٣
OUTPUT	EFFDIA	D _c	EFFECTIVE PARTICLE DIAMETER DERIVED FROM SPECIFIC SURFACE AREA	۳
OUTPUT	ELVMC	(2)	MOLTEN CORE REGION ELEVATION AT LOWER BOUNDARY	м
OUTPUT	ESTOT	(2)	ESTIMATED TIME OF DISRUPTION	s
OUTPUT	HYDGC	(1)	HYDRUGEN GENERATION DURING DELTT	MALES
OUTPUT	INI	(2)	COHESIVE DEBRIS REGION TYPE	
DUTPUT	KTERMC	(2)	FLAG TO INDICATE NORMALITY OF RUN	
OUTPUT	POROPC	ΔP	PRESSURE DROP ACRUSS THE COHESIVE BED	PA
DUTPUT	POROSC	E.	AVERAGE COHESIVE BED POROSITY	
OUTPUT	RBORPT	(2)	DISRUPTION FLAG	
OUTPUT	THMOTC	(2)	MOLTEN MATERIAL THICKNESS	
OUTPUT	VELFTC	(2)	VELOCITY OF MOLTON POOL FLOWING DOWNWARD	4/5
DUTPUT	YCHRL	1	CHARACTERISTIC LENGTH OF FROZEN BED	м

(1) Variables that are currently inactive.

(2) Variables are not shown in Section 2.

TABLE 6. INPUT/OUTPUT DESCRIPTION FOR DBFRAG

USE	FORTRAN	SYMBOL	DESCRIPTION	UNITS
INPUT	ABSMR	M _{Ab}	TOTAL MASS OF CONTROL ROD MATERIAL ACCUMULATED	ĸG
INPUT	ALPHAR	(1)	EFFECTIVE ALPHA-ZR REACTION AREA	M2
INPUT	ALPHTR	(1)	EFFECTIVE ALPHA-ZR REACTION LAYER THICKNESS	м
INPUT	AREAR	A _r	TOTAL BUNDLE CROSS SECTIONAL AREA IN DEBRIS	M2
TUPHT	DELTT	Δt	TIME STEP	5
INPUT	ELVNR	(2)	ELEVATION OF RUBBLE BODY-FROM THE BOTTOM OF ROD BUNDLE TO THE BOTTOM OF RUBBLE BODY REGION	*
NPUT	HITRG	Hnd	FRAGMENTED DEBRIS REFION HEIGHT FROM DBREGN	м
INPUT	HTLBRC	HTLBCC	HEAT TRANSFER INTO RUBBLE DEBRIS COOLANT AT	41m2
INPUT	HTLBRD	HTLBCD	HEAT TRANSFER INTO RUBBLE DEBRIS BED AT LOJER BOUNDARY	W/MZ
INPUT	HTUBRC	HTUBCC	HEAT TRANSFER INTO RUBBLE DEBRIS COOLANT AT	W/M2
INPUT	HTUBRD	HTUBCD	HEAT TRANSFER INTO RUBBLE DEBRIS BED AT UPPER BUUNDARY	4/M2
INPUT	I	(2)	INDEX OF CURRENT TIME FROM TIME ARRAY	
INPUT	MAXL	(2)	MAXIMUM NUMBER OF NODES IN THE DEBRI'S REGION WHICH COMBINED LIQUID, SATURATION, AND VAPOR REGION	
INPUT	ND	nd	NUMBER OF NODES TO BE USED IN LIQUID OR VAPOR REGION FOR DEBRIS REGION	
INPUT	NTIME	(2)	NUMBER OF TIME STEPS IN TIME ARRAY	

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TABLE 6. (CONTINUED)

USE	FORTRAN	SYMBOL	DESCRIPTION	21140
INPUT	SIZAVR	D _r	AVERAGE PARTICLE SIZE OVER ACCUMULATED MASS AND COMPONENTS IN RUBBLE DEBRIS BED	
INPUT	STRMR	M _{St}	TOTAL MASS OF CORE STRUCTURE MATERIALS ACCUMULATED IN RUBBLE DEBRIS BED	ĸG
INPUT	T	(2)	TIME STEP ARRAY	s
INPUT	UO2MR	Mu02	TOTAL MASS OF UD2 ACCUMULATED FOR ALL COMPONENTS	ĸG
INPUT	VINR	u _o	COJLANT INLET VELOCITY AT BOTTOM OF DEBRIS	M/S
INPUT	VINROD	(2)	COOLANT INLET VELOCITY AT BOTTOM OF DEBRIS REGION AT PREVIOUS TIME STEP	4/5
INPUT	XMASSR	(2)	TOTAL MASS OF DEBRIS ACCUMULATED FOR ALL COMPONENTS IN RUBBLE DEBRIS BED	κG
INPUT	ZRMR	MZr	TOTAL MASS OF ZIRCALOY ACCUMULATED FOR ALL COMPONENTS IN RUBBLE DEBRIS BED	κG
INPUT	ZRO2MR	MZr02	TUTAL MASS OF ZRO2 ACCUMULATED FOR ALL COMPONENTS IN RUBBLE DEBRIS BED	۴G
INPUT	ZRG2TR	(1)	EFFECTIVE ZRO2 REACTION LAYER THICKNESS	м
1/0	BEDTMK	T	DEBRIS TEMPERATURE CORRESPONDING TO NONR NODES	к
1/0	COLTMR	T	COULANT TEMPERATURE CORRESPONDING TO NONR NODES	×
1/0	ELVAR	(2)	ELEVATION OF AXIAL NODES IN DEBRIS	
1/0	ELVMR	(2)	MOLTEN CORE REGION ELEVATION AT LOWER BOUNDARY	м
I/0	FISHR	(1)	FISSION/DECAY HEAT GENERATION RATE	W/M3
1/0	IDREGR	IDREGN	REGION TYPE ID	

TABLE 6. (CONTINUED)

USE	FORTRAN	SYMBUL	DESCRIPTION	UNITS
1/0	NONR	NOND	NUMBER OF AXIAL NODES USED IN DEBRIS REGION ANALYSIS	
1/0	OXDAR	(1)	ZR-STEAM HEAT GENERATION RATE	W/M3
OUTPUT	CURTIM	(2)	CURRENT TIME	S
UUTPUT	DOWNR	(2)	LENGTH OF MOLTEN POOL PENETRATION	M
DUTPUT	ESTOT	(2)	ESTIMATED TIME OF DISRUPTION	S
TUATO	HITER	Hr, Lf	RUBBLE BED HEIGHT	м
DUTPUT	IRT	(2)	DEBRIS REGION TYPE	
OUTPUT	KFLUID	(2)	FLUIDIZATION FLAG, =D PACKED BED, =1 FLUIDIZED BED	
OUTPUT	KTERM	(2)	ABNORMAL TERMINATION FLAG	
JUTPUT	PDROPR	ΔP	PRESSURE DROP ACRUSS THE RUBBLE DEBRIS BED	PA
OUTPUT	POROSR	E,	AVERAGE RUBBLE BED PUROSITY	
OUTPUT	PBDRPT	(2)	DISRUPTION FLAG	
JUTPUT	THROTR	(2)	MOLTEN MATERIAL THICKNES	
JUTPUT	VELMOT	(2)	VELOCITY OF MOLTEN POOL FLOWING DOWNWARD	115
OUTPUT	XCHRL	1 _r	CHARACTERISTIC LENGTH OF THE PARTICLE IN RJBBLE DEBRIS BED	•

Variables that are currently inactive.

(2) Variables are not shown in Section 2.

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USE	NAME	SYMBOL	DESCRIPTION	JNITS
INPUT	DELTIN	(2)	TIME STEP CALCULATED IN THE DISRUPTED BUNDLE	5
INPUT	NSTP	(2)	NUMBER OF STEPS IN WHICH DISRUPTED BUNDLE TIME STEP WILL BE BROKEN	
OUTPUT	DELTOT	(2)	TIME STEP TO BE USED IN DEBRIS ANALYSIS	S.

TABLE 7. INPUT/OUTPUT DESCRIPTION FOR FRTIME

TABLE 8. INPUT/OUTPUT DESCRIPTION FOR FRCHAR

USE	FORTRAN	SYMBOL	DESCRIPTION	UNITS
INPUT	ABSMC	M _{Ab}	TOTAL MASS OF CONTROL ROD MATERIAL ACCUMULATED	КG
INPUT	AREAR	A _c	TOTAL BUNDLE CROSS SECTIONAL AREA IN DEBRIS	M 2.
INPUT	DELTC	Δt	TIME STEP FOR COHESIVE DEBRIS REGION	S
INPUT	HITEC	Hc	FROZEN DEBRIS REGION HEIGHT FROM DBREGN	м
INPUT	ROABS	PAb	DENSITY OF CONTROL KOD MATERIAL FOR DEBRIS REGION	KGIMB
INPUT	ROCOL .	Pc	CODLANT DENSITY AT BUTTOM OF DEBRIS	KGINB
INPUT	RUSTR	PSt	DENSITY OF STRUCTURAL MATERIAL FOR DEBRIS REGION	K 67 M 3
INPUT	ROUDZ	ρμο	UU2 DENSITY	KGIMB
INPUT	ROZR	P7r	ZR DENSITY	KG/M3
INPUT	ROZRU2	P7r0	ZRU2 DENSITY	KGIMB
INPUT	STRMC	M _{St} ²	TOTAL MASS OF CORE STRUCTURAL MATERIALS ACCUMULATED IN COHESIVE DEBRIS BED	KG
IUGNI	JMSEU	MUO2	TOTAL MASS OF UD2 ACCUMULATED FOR ALL COMPONENTS IN COHESIVE DEBRIS BED	K G
INPUT	VINC	u _o	CODLANT VELOCITY AT BOTTOM OF COHESIVE DEBRIS REGION	MIS
INPUT	VINCOD	(2)	CODLANT VELOCITY AT BOTTOM OF COMESIVE DEBRIS REGION AT PREVIOUS TIME STEP	MV S
INPUT	XMASSC	(2)	TOTAL MASS OF DEBRIS ACCUMULATED FOR ALL COMPONENTS IN COHESIVE DEBRIS BED	KG
INPUT	XMUCOL	μ	VISCOSITY OF COOLANT AT BOTTOM OF DEBRIS	KG/SEC/M

TABLE 8. (CONTINUED)

USE	FURTKAN NAME	S Y MB DL	DESCRIPTION	UNITS
INPUT	ZRMC	Mzr	TOTAL MASS OF ZR ACCUMULATED FOR ALL COMPONENTS	КG
INPUT	ZROZNC	MZr02	TOTAL MASS OF ZRUZ ACCUMULATED FOR ALL COMPONENTS IN CUHESIVE DEBRIS BED	κG
UUTPUT	EFFDIA	D _c	EFFECTIVE PARTICLE DIAMETER DERIVED FROM SPECIFIC SURFACE AREA	м
JUTPUT	KTERMC	(2)	FLAG TO INDICATE NORMALITY OF RUN	
TUTPUT	PDROFC	ΔP	PRESSURE DROP ACROSS THE COHESIVE BED	PA
TUTTU	PURDSC	E	AVERAGE COHESIVE BED POROSITY	
DUTPUT	YCHRL	1 _r	CHARACTERISTIC LENGTH OF FROZEN BED	м
(1) Vari	ables that	are curren	tly inactive.	
(2) Vari	ables are n	ot shown in	n Section 2.	

USE	FURTRAN	SYMBOL	DESCRIPTION	UNITS
INPUT	ALPHAC	(1)	EFFECTIVE ALPHA-ZR REACTION AREA	M2
INPUT	ALPHTC	(1)	EFFECTIVE ALPHA-ZR REACTION LAYER THICKNESS	м
INPUT	BEDTMP	Тр	DEBRIS BED TEMPERATURE CORRESPONDING TO AXIAL NODES	к
INPUT	COLIMP	т _с	DEBRIS BED COULANT TEMPERATURE CORRESPONDING TO AXIAL NODES	к
INPUT	DELIT	Δt	TIME STEP	S
INPUT	EFFDIA	D _c	EFFECTIVE PARTICLE DIAMETER DERIVED FROM SPECIFIC SURFACE AREA	M
INPUT	ELVAY	(2)	ELEVATION OF DEBRIS AXIAL NODES	н.
INPUT	ELVNC	(2)	ELEVATION OF POROUS BODY-FROM THE BOTTOM OF ROD BUNDLE TO THE BOTTOM OF POROUS BODY REGION	м
INPUT	FISHC	(1)	FISSION DECAY HEAT GENERATION RATE	W/M3
INPUT	HITEC	H _c	FROZEN DEBRIS REGION HEIGHT FROM DBREGN	M
INPUT	HTLBCC	HTLBCC	HEAT TRANSFER INTO COHESIVE DEBRIS COOLANT AT	w/M2
INPUT	HTLBCD	HTLBCD	HEAT TRANSFER INTO COHESIVE DEBRIS BED TO LOWER BOUNDARY	W/ M2
INPUT	HTUBCC	HTUBCC .	HEAT TRANSFER INTO COHESIVE DEBRIS COOLANT AT	w/M2
INPUT	HTUBCD	HTUBCD	HEAT TRANSFER INTO COHESIVE DEBRIS BED AT UPPER BOUNDARY	W/ M2
INPUT	IDREGN	IDREGN	DEBRIS REGION ID NUMBER OF LAST TIME STEP	
INPUT	MAXL	(2)	MAXIMUM NUMBER OF NJDES IN THE DEBRIS REGION WHICH COMBINED LIGUID, SATURATION, AND VAPOR REGION	

TABLE 9. (CONTINUED)

USE	FORTRAN	SYMBOL	DESCRIPTION	UNITS
INPUT	ND	nd	NUMBER OF NODES TO BE USED IN LIQUID JR VAPOR REGION FOR DEBRIS REGION	
INPUT	NUND	NOND	NUMBER OF TOTAL NODES IN THE ANALYSIS	
INPUT	DADAC	(1)	ZR-STEAM HEAT GENERATION RATE	w/M3
INPUT	POKOSC	ε _c	AVERAGE COHESIVE BED PORDSITY	
INPUT	VINC	uo	COOLANT VELOCITY AT BOTTOM OF COHESIVE DEBRIS	MIS
INPUT	YCHRL	1	CHARACTERISTIC LENGTH OF FROZEN BED	м
INPUT	ZROZAC	(1)	EFFECTIVE ZR-STEAM REACTION AREA	M 2
INPUT	ZROZTC	(1)	EFFECTIVE ZROZ REACTION LAYER SHICKNESS	м
DUTPUT	BEDTMP	тр	DEBRIS BED TEMPERATURE CORRESPONDING TO AXIAL NODES	×
DUTPUT	COLTHP	т _с	DEBRIS BED CODLANT TEMPERATURE CURRESPONDING TO AXIAL NODES	к
TUY FUT	DJWNZ	(2)	LENGTH OF MOLTEN POOL PENETRATION IN COHESIVE DEBRIS	Μ
TUTTUE	ELVAY	(2)	ELEVATION OF DEBRIS AXIAL NODES	м
DUTPUT	ELVMC	(2)	MOLTEN CORE REGION ELEVATION AT LOWER BOUNDARY	м
TUALO	FGRSC	(1)	FISSION GAS RELEASE DURING DELTT	MOLES
JUTPUT	FISHC	(1)	FISSION DECAY HEAT GENERATION RATE	w/ M3
JUTPUT	HYDGC	(1)	HYDRUGEN GENERATION DURING DELTT	MOLES
JUTPUT	IDREGN	IDREGN	DEBRIS REGION ID NUMBER OF LAST TIME STEP	
JUTPUT	INT	(2)	COHESIVE DEBRIS REGION TYPE	

TABLE 9. (CONTINUED)

USE	FORTRAN	SYMBOL	DESCRIPTION	UNITS
OUTPUT	NOND	NOND	NUMBER OF TOTAL NODES IN THE ANALYSIS	
UUTPUT	DXDAC	(1)	ZR-STEAM HEAT GENERATION RATE	W/M3
DUTPUT	THMOTC	(2)	MOLTEN MATERIAL THICKNESS	м
UUTPUT	VOLGSC	(1)	VOLATILE FISSION PRODUCTS RELEASE FURING DELTT	MOLE
(1) Vari	ables that	are curren	tly inactive.	
(2) Vari	ables are n	ot shown i	n Section 2.	

TABLE 10. INPUT/OUTPUT DESCRIPTION FOR FRMELT

USE	FURTRAN NAME	SYMBUL	DESCRIPTION	UNITS
INPUT	DELTC	Δt	TIME STEP FOR COHESIVE DEBRIS REGION	S
INPUT	ELVAY	(2)	ELEVATION OF DEBRIS AXIAL NODES	м
INPUT	ELVMC	(2)	MOLTEN CORE REGION ELEVATION AT LOWER BOUNDARY	M
INPUT	IMT	(2)	COHESIVE DEBRIS REGION TYPE	
INPUT	NUND	NOND	NUMBER OF TOTAL NODES IN THE ANALYSIS	
DUTPUT	VELMIC	(2)	VELOCITY OF MOLTUN POOL FLOWING DOWNWARD	M/S

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(2) Variables are not shown in Section 2.

TABLE 11. INPUT/OUTPUT DESCRIPTION FOR FRESTT

USE	NAME	SYMBOL	DESCRIPTION	UN115
INPUT	CURTIM	(2)	CURRENT TIME	S
INPUT	ELVMC	(2)	MOLTEN CORE REGION ELEVATION AT LOWER BOUNDARY	м
INPUT	ELVNC	(2)	ELEVATION OF POROUS BODY-FROM THE BOITOM OF ROD BUNDLE TO THE BOTTOM OF POROUS BODY REGION	м
INPUT	VELMIC	(2)	VELOCITY OF MOLTON POOL FLOWING DOWNWARD	MIS
DUTPUT	ESTOT	(2)	ESTIMATED TIME OF DISRUPTION	S
(1) Var	ables that	are curren	tly inactive.	
(2) Var	iables are n	ot shown i	n Section 2.	

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USE	FURTRAN NAME	SYMBUL	DESCRIPTION	UNITS
INPUT	DELTIN	(2)	TIME STEP CALCULATED IN THE DISRUPTED BUNGLE	s
INPUT	NSTP	(2)	NUMBER OF STEPS IN WHICH DISRUPTED BUNDLE TIME STEP WILL BE BROKEN	
OUTPUT	DELTOT	(2)	TIME STEP TO BE USED IN DEBRIS ANALYSIS	S

TABLE 12. INPUT/OUTPUT DESCRIPTION FOR FGTIME

TABLE 13. INPUT/OUTPUT DESCRIPTION FOR FGCHAR

USE	FORTRAN	SYMBOL	DESCRIPTION	UNITS
INPUT	ABSMR	M _{Ab}	TUTAL MASS OF CONTROL ROD MATERIAL ACCUMULATED	КG
INPUT	AREAR	A _r	TOTAL BUNDLE CRUSS SECTIONAL AREA IN DEBRIS REGION	M2
INPUT	DELTR	Δt	TIME STEP FOR DEBRIS REGION	S
INPUT	HITKG	Hrd	FRAGMENTED DEBRIS REFION HEIGHT FROM DBREGN	М
INPUT	RUABS	PAb	DENSITY OF CONTROL ROD MATERIAL FOR DEBRIS REGION	KG/M3
INPUT	ROCOL	ρ	COULANT DENSITY AT BUTTOM OF DEBRIS	KG/M3
INPUT	ROSTK	PSt	DENSITY OF STRUCTURAL MATERIAL FOR DEBRIS REGION	K 61 M3
INPUT	ROUD2	ριιο	UU2 DENSITY	KGIM3
INPUT	RUZR	P72	ZR DENSITY	K G/ M3
INPUT	ROZROZ	P7r0	ZRO2 DENSITY	KGIMB
INPUT	SIZAVR	D _r ²	AVERAGE PARTICLE SIZE OVER ACCUMULATED MASS AND COMPONENTS IN RUBBLE DEBRIS BED	м
INPUT	STRMP	M _{St}	TOTAL MASS OF CORE STRUCTURE MATERIALS ACCUMULATED IN RUBBLE DEBRIS BED	ĸб
INPUT	UU2MR	Mu02	TOTAL MASS OF 002 ACCUMULATED FOR ALL COMPONENTS IN RUBBLE DEBRIS BED	КG
INPUT	VINR	u _o	COOLANT INLET VELOCITY AT BOTTOM OF DEBRIS	MIS
INPUT	VINREE	(2)	CODLANT INLET VELOCITY AT BOTTOM OF DEBRIS REGION AT PREVIOUS TIME STEP	MIS
INPUT	XMASSR	(2)	TOTAL MASS OF DEBRIS ACCUMULATED FOR ALL	КG

TABLE 13. (CONTINUED)

NAME	SYMBOL	DESCRIPTION	UNITS
XMUCOL	μ	VISCOSITY OF CODLANT AT BOTTOM OF DEBRIS	KG/SEC/M
ZRMP	MZr	TOTAL MASS OF ZIRCALDY ACCUMULATED FOR ALL COMPONENTS IN RUBBLE DEBRIS BED	κG
ZRO2MR	MZr02	TOTAL MASS OF ZRU2 ACCUMULATED FOR ALL COMPONENTS IN RUBBLE DEBRIS BED	КG
HLTER	L,H	RUBBLE BED HEIGHT	м
KFLU1D	(2)	FLUIDIZATION FLAG, =0 PACKED BED, =1 FLUIDIZED BED	
KTERM	(2)	ABNORMAL TERMINATION FLAG	
PURGPR	ΔP	PRESSURE DRUP ACROSS THE RUBBLE DEBRIS BED	PA
PORUSE	ε,	AVERAGE RUBBLE BED POROSITY	
XCHEL	1 _r	CHARACTERISTIC LENGTH OF THE PARTICLE IN RUBBLE DEBRIS BED	м
ables that	are curren	tly inactive.	
	XMUCOL ZRMR ZRO2MR HITER KFLU1D KTERM POROPR POROSK XCHRL ables that	AME SYMBOL XMUCOL μ ZRMP M_{Zr} ZRO2MR M_{ZrO_2} HITER L _f ,H _r KFLU1D (2) KTERM (2) PURUPR ΔP PURUSK ε_r XCHKL 1_r ables that are curren	NAME SYMBOL DESCRIPTION XMUCOL μ VISCOSITY OF CODLANT AT BOTTOM OF DEBRIS ZRMR MZr TOTAL MASS OF ZIRCALDY ACCUMULATED FOR ALL ZROZMR MZrO2 TOTAL MASS OF ZROZACCUMULATED FOR ALL ZROZMR MZrO2 TOTAL MASS OF ZRUZ ACCUMULATED FOR ALL LITER LF,Hr RUBBLE BED HEIGHT KFLUID (2) FLUIDIZATION FLAG, =O PACKED BED, =1 FLUIDIZED KTERM (2) ABNORMAL TERMINATION FLAG POROFR ΔP PRESSURE DROP ACROSS THE RUBBLE DEBRIS BED POROFR ΔP POROFR ΔP POROFR ΔP BED AVERAGE RUBBLE BED POROSITY XCHKL 1r CHARACTERISTIC LENGTH OF THE PARTICLE IN RUBBLE BEBRIS BEO ables that are currently inactive.

ušE	FORTRAN	SYMBOL	DESCRIPTION	UNITS
INPUT	ALPHAR	(1)	EFFECTIVE ALPHA-ZR REACTION AREA	M 2
INPUT	ALPHIR	(1)	EFFECTIVE ALPHA-ZR REACTION LAYER THICKNESS	M
INPUT	AREAK	A _r	TOTAL BUNDLE CRUSS SECTIONAL AREA IN DEBRIS REGION	12
INPUT	DELTK	Δt	TIME STEP FOR DEBRIS REGION	S
INPUT	ELVNR	(2)	ELEVATION OF RUBBLE BODY-FROM THE BOTTOM OF ROD BUNDLE TO THE BOTTOM OF RUBBLE BODY REGION	м
INPUT	HITER	Hr, Lf	RUBBLE BED HEIGHT	м
INPUT	HTLBRC	HTLBCC	HEAT TRANSFER INTO RUBBLE DEBRIS COOLANT AT	N/M2
INPUT	HTLBED	HTLBCD	HEAT TRANSFER INTO RUBBLE DEBRIS BED AT LOWER BOUNDARY	W/M2
INPUT	HTUBKC	HTUBCC	HEAT TRANSFER INTO RUBBLE DEBRIS COOLANT AT	w/ M2
INPUT	HTUBRD	HTUBCD	HEAT TRANSFER INTO RUBBLE DEBRIS BED AT UPPER BOUNDARY	W/M2
INPUT	KFLUID	(2)	FLUIDIZATION FLAG, =0 PACKED BED, =1 FLUIDIZED BED	
INPUT	MAXL	(2)	MAXIMUM NUMBER OF NODES IN THE DEBRIS REGION WHICH COMBINED LIQUID, SATURATION, AND VAPOR REGION	
INPUT	ND	nd	NUMBER OF NODES TO BE USED IN LIQUID OR VAPOR Region for debris region	
INPUT	PORDSR	ε _r	AVERAGE RUBBLE BED PORUSITY	
INPUT	SIZAVR	D _r	AVERAGE PARTICLE SIZE OVER ACCUMULATED MASS AND COMPONENTS IN RUBBLE DEBRIS BED	м

TABLE 14. (CONTINUED)

USE	FORTRAN	SYNBOL	DESCRIPTION	UNITS
1420.1	/ INR	u _o	COULANT INLET VELOCITY AT BOTTOM OF DEBRIS. REGION	MZ S
INPUT	XCHRL	¹ r	CHARACTERISTIC LENGTH OF THE PARTICLE IN RUBBLE DEBRIS BED	m
INPUT	ZROZAR	(1)	EFFECTIVE ZR-STEAM REACTION AREA	M2
INPUT	ZRUZTR	(1)	EFFECTIVE ZEOZ REACTION LAYER THICKNESS	м
DUTPUT	BEDTMR	T	DEBRIS TEMPERATURE CORRESPONDING TO NONR NODES	
DUTPUT	COLIME	T	COOLANT TEMPERATURE CORRESPONDING TO NONE NODES	
DUTPUT	DOWNR	(2)	LENGTH OF NOLTEN POUL PENETRATION	M
UTPUT	ELVAR	(2)	ELEVATION OF AXIAL NODES IN DEBKIS	
TUTI	CLVMR	(2)	MOLTEN CORE REGION ELEVATION AT LOWER BOUNDARY	M
TUTTU	FGRSR	(2)	FISSION GAS KELEASE (MOLES) DURING DELTR	
JUTPUT	FISHR	(1)	FISSION/DECAY HEAT GENERATION RATE	W/ M3
TUTTU	HYDGH	(1)	MYDRIGEN GENERATION DURING DELTR	MOLES
JUTPUT	IDREGR	IDREGN	REGION TYPE ID	
JUTPUT	IRT	(2)	DEBRIS REGION TYPE	
UUTPUT	NONP	NOND	NUMBER OF AXIAL NODES USED IN DEBRIS REGION ANALYSIS	
OUTPUT	OXDAR	(1)	AR-STEAM HEAT GENERATION RATE	W/M3
JUTPUT	TESTBB	(2)	ESTIMATED TIME STEP FOR LOWER BOUNDARY BREAKTHROUGH AFTER CURRENT TIME	5
DUTPUT	THMOTP	(2)	MULTEN MATERIAL THICKNES	M

TABLE 14. (CONTINUED)

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USE	NAME	SYMBOL	DESCRIPTION	cTINU
DUTPUT	VELMET	(2)	VELOCITY OF MULTEN POOL FLOWING DOWNWARD	MIS
DUTPUT	VOLGSR	(1)	VOLATILE FISSION PRODUCTS RELEASE DURING DELTR	MOLE
(1) Varia	ables that	are curren	tly inactive.	

TABLE 15. INPUT/OUTPUT DESCRIPTION FOR FGMELT

USE	FORTRAN	SYMBOL	DESCRIPTION	UNITS
INPUT	DELTR	Δt	TIME STEP FOR DEBKIS REGION	5
INPUT	ELVAR	(2)	ELEVATION OF AXIAL NODES IN DEBRIS	
INPUT	ELVMR	(2)	MOLTEN CORE REGION ELEVATION AT LOWER BOUNDARY	M
NPUT	IRT	(2)	DEBRIS REGIUN TYPE	*
TUSN	NONR	NOND	NUMBER OF AXIAL NODES USED IN DEBRIS REGION ANALYSIS	
TUTTU	VELMOT	(2)	VELOCITY OF MOLIEN POOL FLOWING DOWNWARD	MIS
1) Vari	ables that	are curren	tly inactive.	
(2) Vari	ables are n	ot shown i	n Section 2.	

TABLE 16. INPUT/OUTPUT DESCRIPTION FOR FGESTT

USE	FORTRAN	SYMBOL	DESCRIPTION	UNITS
INPUT	CUNTIM	(2)	CURRENT TIME	s
INPUT	ELVMK	(2)	MOLTEN CORE REGION ELEVATION AT LOWER BOUNDARY	n
INPUT	LLVNR	(2)	ELEVATION OF RUBBLE BODY-FROM THE BOTTOM OF ROD BUNDLE TO THE BOTTOM OF RUBBLE BODY REGION	м
INPUT	VELMOT	(2)	VELOCITY OF MOLTEN POOL FLOWING DOWNWARD	11/5
TPUT	ESTDT	(2)	ESTIMATED TIME OF DISRUPTION	S

TABLE 17.	INPUT/OUTPUT	DESCRIPTION	FOR DRYOUT
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USE	NAME	SYMBOL	DESCRIPTION	UNITS
INPUT	EFFDIA	d	EFFECTIVE PARTICLE DIAMETER DERIVED FROM SPECIFIC SURFACE AREA	м
NPUT	HFG	hfa	LATENT HEAT OF VAPORIZATION	JIKG
INPUT	HITEC	H	FROZEN DEBRIS REGION HEIGHT FROM DBREGN	м
NPUT	POROPC	ΔP	PRESSURE DROP ACRUSS THE COHESIVE BED	PA
NPUT	POROSC	ε	AVERAGE COHESIVE BED POROSITY	
NPUT	QVUL	Q	VOLUMETRIC HEAT GENERATION RATE	#/M3
NPUT	RUCOL	ρ1	COOLANT DENSITY AT BUTTOM OF DEBRIS	KG/M3
NPUT	RUVAP	P	VAPOR DENSITY	KGIMB
NPUT	SURTC	σ	SURFACE TENSION OF COOLANT	PA
NPUT	VINC	u _o	COOLANT VESOCITY AT BOTTOM OF COHESIVE DEBRIS REGION	MIS
NPUT	XMUCOL	μ	VISCOSITY OF COULANT AT BUTTOM OF DEBRIS	KG/SEC/
NPUT	XMUVAP	μ	VAPOR VISCOSITY	KG/SE/M
UTPUT	QUYOUT	q.	DRYOUT HEAT FLUX	W/M2

. . .

(1) Variables that are currently inactive.

(2) Variables are not shown in Section 2.

USE	NAME	SYMBOL	DESCRIPTION	UNITS
INPUT	BEDINP	т _р	DEBRIS BED TEMPERATURE CORRESPONDING TO AXIAL NODES	ĸ
INPUT	COLIMP	T _c	DEBRIS BED COULANT TEMPERATURE CORRESPONDING TO AXIAL NODES	к
INPUT	ELVAY	(2)	ELEVATION OF DEBRIS AXIAL NODES	м
INPUT	ELVNC	(2)	ELEVATION OF POROUS BODY-FROM THE BOITOM OF ROD BUNDLE TO THE BOTTOM OF POROUS BODY REGION	M
INPUT	HITEC	Hc	FROZEN DEBRIS REGION HEIGHT FROM OBREGN	м
INPUT	IOR	(2)	REGION ID NUMBER CALCULATED IN FROZTH OR FRAGTH	
NPUT	IDREGN	IDREGN	DEBRIS REGION ID NUMBER OF LAST TIME STEP	
INPUT	MAXL	(2)	MAXIMUM NUMBER OF NODES IN THE DEBRIS REGION WHICH COMBINED LIQUID, SATURATION, AND VAPOR REGION	
INPUT	ND	nd	NUMBER OF NODES TO BE USED IN LIQUID ON VAPOR REGION FOR DEBRIS REGION	
INPUT	NOND	NOND	NUMBER OF TOTAL NUDES IN THE ANALYSIS	
INPUT	ISAT	T _{cat}	CODLANT SATURATION TEMPERATURE	к
INPUT	XLLIQ	L	LIQUID REGION LENGTH	м
INPUT	XLSAT	L	SATURATION REGION LENGTH	М .
INPUT	XLVAP	L	VAPOR REGION LENGTH	м
DUTPUT	BEDTMP	Tp	DEBRIS BED TEMPERATURE CORRESPONDING TO AXIAL NODES	к
UUTPUT	COLIMP	Т _с	DEBRIS BED CUULANT TEMPERATURE CORRESPONDING TO AXIAL NODES	ĸ
TABLE 18. (CONTINUED)

USE	FORTRAN	SYMBOL			DESCR	IPTION	STINU
	T ELVAY	(2)	ELEVATION O	F DEBRIS	AXIAL	NODES	n
(1)	Variables that	200 00000	tly inactive				
(1)	variables that	are curren	ciy mactive.				
(2)	Variables are i	not shown i	n Section 2.				

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TABLE 19. INPUT/OUTPUT DESCRIPTION FOR TEMPSR

USE	FORTRAN	SYMBOL	DESCRIPTION	UNITS
INPUT	DELTT	Δt	TIME STEP	s
INPUT	DELTZ	Δz	DISTANCE BETWEEN AXIAL NODE	м
INPUT	HTLBCC	HTLBCC	HEAT TRANSFER INTO COHESIVE DEBRIS COOLANT AT LOWER BOJNDARY	W/M2
INPUT	HTLBCD	HTUBCD	HEAT TRANSFER INTO COHESIVE DEBRIS BED TO LOWER BOUNDARY	W/M2
INPUT	H.JBCC	HTUBCC	HEAT TRANSFER INTO COHESIVE DEBRIS COOLANT AT	W/M2
INPUT	нтивсо	HTUBCD	HEAT TRANSFER INTO COHESIVE DEBRIS EED AT UPPER BOUNDARY	W/M2
INPUT	HVSC	Ηv	HEAT TRANSFER COEFFICIENT BETWEEN BOD AND COBLANT, VOLUMETRIC	W/K/M3
INPUT	IDYOT	(2)	INDICATOR OF COULANT STATE	
INPUT	N	nd	NUMBER OF AXIAL NODES	
INPUT	N2	2 · nd	2N FOR SULVING COULANT AND BED TEMPERATURE SIMULIANEOUSLY	
INPUT	POROSC	ε	AVERAGE COHESIVE BED PORDSITY	
INPUT	OVOL	Q'''	VOLUMETRIC HEAT GENERATION RATE	W/M3
INPUT	TCOLCO	Т _с	COULANT TEMPERATURE AT N NODES AT PREVIOUS TIME STEP	к
INPUT	TEMPCO	Tp	BED TEMPERATURE AT N NODES AT PREVIOUS TIME STEP	к
INPUT	VINC	uo	CODLANT VELOCITY AT BOTTOM OF COHESIVE DEBRIS	MIS

 $\mathcal{H}_{\mathcal{H}}$

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TABLE 19. (CONTINUED)

USE	FORTRAN	SYMBOL	DESCRIPTION	UNITS
OUTPUT	TCOLC	T	COOLANT TEMPERATURE	ĸ
UUTPUT	TEMPC	Tp	BED TEMPERATURE	к

4. RESULTS OF MODEL ACCEPTANCE TESTING

Testing of models is a necessary part of the process of code development. Deficiencies in logic flow, algebraic errors, and coding errors can be detected through model testing. For the debris characterization and thermal behavior models described in this report, model testing began with a line-by-line verification of all FORTRAN statements. Then, an extensive set of computer runs were performed using all modeling options to fully exploit the possible logic flow paths. Finally, calculational results were evaluated for reasonableness. This was done for each major subroutine. Results of the acceptance testing are discussed in the following sections.

4.1 FRCHAR

Subroutine FRCHAR calculates bed porosity, a characteristic particle length for heat transfer, and pressure drop across a cohesive debris bed. Comparisons of the pressure drop across a porous body calculated with FRCHAR and with hand-calculations using Ergun's correlation [Equation (3)] for various coolant velocities and debris porcsities are shown in Table 20. These data indicate that the code predictions of FHCHAR agree well with Ergun's correlation and that Ergun's correlation is properly implemented in FRCHAR.

4.2 FGCHAR

Subroutine FGCHAR calculates bed height, minimal fluidization velocity, porosity, a characteristic particle length for heat transfer, and pressure drop for a rubble debris bed. The same procedure has been used to check the pressure drop calculations of FGCHAR as was used for subroutine FRCHAR. The results which are shown in Table 21 show excellent agreement. Predictions of minimum fluidization velocity, fluidized bed height, bed porosity, and pressure drop across the bed made using FGCHAR have been checked using the two examples given in Reference 5. Test conditions of these two examples are summarized in Table 22. Comparisons of the FGCHAR results with the two

TABLE 20. TEST RESULTS OF FRCHAR

		(∆P Pa)
Coolant Velocity (m/s)	Debris Bed Porosity	FRCHAR	Hand Calculation
0.01 0.02 0.03 0.04 0.05	0.37 0.37 0.37 0.37 0.37 0.37	7.775×10^{2} 2.254×10^{3} 4.430×10^{3} 7.305×10^{3} 1.088×10^{4}	7.775×10^{2} 2.254×10^{3} 4.430×10^{3} 7.305×10^{3} 1.088×10^{4}
0.06 0.07 0.08 0.09 0.10	0.37 0.37 0.37 0.37 0.37 0.37	$\begin{array}{rrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrr$	1.515 x 104 2.013 x 104 2.580 x 104 3.217 x 104 3.924 x 104
0.14 0.01 0.02 0.03 0.04	0.37 0.104 0.104 0.104 0.104	7.451 x 104 4.329 x 104 1.163 x 105 2.246 x 105 3.627 x 105	7.451 x 104 4.328 x 104 1.181 x 105 2.246 x 105 3.625 x 105
0.05 0.06 0.07 0.08 0.09	0.104 0.104 0.104 0.104 0.104	5.323 × 10 ⁵ 7.335 × 10 ⁵ 9.663 × 10 ⁵ 1.231 × 10 ⁶ 1.527 × 10 ⁶	5.321 x 105 7.333 x 105 9.660 x 105 1.230 x 105 1.526 x 106
0.10 0.14	0.104 0.104	1.854 x 106 3.480 x 105	1.854 x 106 3.479 x 106

TABLE 21. TEST RESULTS OF FRCHAR

		۵ (P	P a)
Coolant Velocity (m/s)	Debris Bed <u>Porosity</u>	FRCHAR	Hand Calculation
0.001 0.002 0.003 0.004 0.005	0.37 0.37 0.37 0.37 0.37 0.37	4.629 x 101 9.957 x 101 1.598 x 102 2.271 x 102 3.014 x 102	4.629 x 101 9.957 x 101 1.599 x 102 2.271 x 102 3.014 x 102
0.006 0.007 0.008 0.009 0.010	0.37 0.37 0.37 0.37 0.37 0.37	3.826×10^{2} 4.709×10^{2} 5.661×10^{2} 6.683×10^{2} 7.775×10^{2}	3.826 x 10 ² 4.709 x 10 ² 5.661 x 10 ² 6.683 x 10 ² 7.775 x 10 ²
0.015 0.020 0.0001 0.0002 0.0003	0.37 0.37 0.45 0.45 0.45	$\begin{array}{rrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrr$	$\begin{array}{c} 1.429 \times 10^{3} \\ 2.254 \times 10^{3} \\ 8.503 \times 10^{1} \\ 1.703 \times 10^{2} \\ 2.557 \times 10^{2} \end{array}$
0.0004 0.0005 0.0006 0.0007 0.0008	0.45 0.45 0.45 0.45 0.45	3.414 × 10 ² 4.272 × 10 ² 5.133 × 10 ² 5.996 × 10 ² 6.860 × 10 ²	3.414 x 10 ² 4.272 x 10 ² 5.133 x 10 ² 5.996 x 10 ² 6.860 x 10 ²
0.0009 0.0010 0.0020 0.0030 0.0040	0.45 0.45 0.45 0.45 0.45	7.727 x 10 ² 8.596 x 10 ² 1.740 x 10 ³ 2.641 x 10 ³ 3.563 x 10 ³	7.727 x 10 ² 8.596 x 10 ² 1.740 x 10 ³ 2.641 x 10 ³ 3.563 x 10 ³

[10] D. Millard, J. M. Karl, M. Ballov, C. M. Markov, N. M. Markov, and M. Markov, Annual Phys. Rev. Lett. 71, 100 (1997).	the second se	and the statement of the
	Example 1	Example 2
Fixed bed beight. M	0.7366	0.7112
Fixed bed nergini,	0.45	0.37
rixed bed porosity	7.493×10^{-4}	4.4196 x 10 ⁻³
Particle average diameter, m	2.547×10^3	1.602×10^3
Particle density, kg/m ⁻	9.98 x 10 ²	9.98 x 10 ²
Coolant density, kg/m°	1.259×10^{-2}	1.244 × 10 ⁻¹
Coolant velocity, m/s	1.30×10^{-3}	1.0×10^{-3}
Coolant viscosity, kg/m•s		

TABLE 22. TEST CONDITIONS OF THE TWO EXAMPLES IN REFERENCE 32

examples are shown in Table 23. The results in Tables 21 and 23 demonstrate that FGCHAR does calculate rubble debris bed characteristics and hydraulic behavior reasonably well for both the packed and fluidized bed configurations, respectively.

4.3 TEMPSR

Debris bed and coolant temperatures are solved simultaneously in the TEMPSR subroutine. Steady state and transient temperature solutions by TEMPSR have been checked by comparison with analytical solutions. Calculated debris bed and coolant temperatures versus time are shown in Figure 4 for the case where the debris bed temperature is initially 2 K greater than that of the overlying coolant. With good heat transfer between debris and coolant (heat transfer coefficient greater than 10^{13} W/m³·K) and no heat generation within the debris, the debris bed and coolant temperatures would be expected to reach an equilibrium temperature state very rapidly. This result is shown to occur in Figure 4 which indicates the TEMPSR calculations have been properly implemented. A second check case was made by assuming a continuous heating of the bed without any heat transfer within the porous system. For such conditions, debris bed temperature increases proportionally to the heating time, as shown in Figure 5. Agreement between the TEMPSK result and the analytical solution is excellent which indicates proper implementation within TEMPSR.

4.4 REGMOD

As discussed in Section 2.2.1, different regions may be used in analyzing debris bed and coolant temperatures, depending on coolant temperature, heat generation rate within the debris, and coolant flow rate. During the temperature calculations, the debris bed and coolant temperature distributions are modified by subroutine REGMOD to correspond to a new nodalization if the assigned region identification number is changed. The temperature distribution of the debris bed and coolant should be identical before and after calling REGMOD although the node number, elevation, and

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	E	xample 1	Exa	ample 2
	FGCHAR	Textbook Solution	FGCHAR	Textbook Solution
Minimum fluidiza- tion velocity, m/s	4.353 x 10 ⁻³	4.302 x 10 ⁻³	2.118 x 10 ⁻²	2.147 x 10 ⁻²
Expanded bed height, m	1.02	1.01	1.99	1.99
Expanded bed porosity	0.60	0.60	0.775	0.775
Pressure drop across the bed, Pa	6.16 x 10 ³	6.15 x 10 ³	2.654 x 10 ³	2.652 x 10 ³

TABLE 23. COMPARISON OF FGCHAR PREDICTIONS WITH TEXTBOOK SOLUTIONS



Figure 4. Comparison of TEMPSR prediction with analytical solution.

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Figure 5. Comparison of TEMPSR prediction with analytical solution.

corresponding temperature may be changed. The interpolation capability of REGMOD for various transitions of region identification number are demonstrated by the results shown in Figures 6 and 7. The excellent agreement shown in Figures 6 and 7 indicates that the interpolation performed by REGMOD is correct.

4.5 FROZTH and FRAGTH

Subroutines FROZTH and FRAGTH compute debris and coolant temperatures and thermally related behavior (melting) of a cohesive and rubble debris bed, respectively. Calculated coolant and debris bed temperature distributions versus time are shown in Figure 8 for a debris bed with the following conditions:

- 1. Debris bed height of 0. m
- 2. Constant volumetric heat generation rate of 3.38 x 10^3 W/m³
- 3. Coolant velocity of 0.001 m/s
- 4. Bed porosity of 0.5208.

Initially the debris bed consists of subcooled, saturated, and superheated regions for the thermal calculations (i.e., IDREGN = 6). As heatup continues and the coolant temperatures exceed the saturation temperature, a superheated region with IDREGN = 2 is used for the thermal analysis.

The thermal response of a packed bed with the same characteristics as the cohesive bed discussed above is expected to be identical to that for the cohesive bed. This analysis was performed with the FRAGTH subroutine, and the results are shown in Figure 9. These results are identical to those shown in Figure 8 which indicates consistency between FROZTH and FRAGTH.



Figure 6. Interpolation of temperature distribution by REGMOD.



Figure 7. Interpolation of temperature distribution by REGMOD.



Figure 8. FROZTH calculation of debris bed and coolant temperature distribution.





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APPENDIX A LISTINGS OF DEBRIS BEHAVIOR MODELS .

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APPENDIX A LISTINGS OF DEBRIS BEHAVIOR MODELS

FORTRAN listings of the subroutines which are used to calculate debris bed characteristics and thermal behavior are given in Tables A-1 through A-15. Listings of DBDR^{TV}, DEBINP, DBTIME, and DBOUTD are given in Tables A-16 through A-19. TABLE A-1. LISTING OF DBFROZ

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1 [=]	1																																														
:1=1	1	н	IL	E		I	• L	T	N																																						
:I=1 :DO	1 *	н	IL	E	TE	I	.L	T	N	s	E	BE	D	с	н	AR	A	CI	TE	R	1	51	I	c	s	I	NC	L	UC	I	N	G	н	rD	RA	U	L	IC	E	361	на	v	IO	R	C F	GCH	R
:I=) :DO	1 + + C + C		IL MP		TE	I	.L DE	B	N	s	8	BE	D	C T	н	R	A	A	TELL	R	1:	ST	I	C:	S	I	NC	E		I	NI	G	н	rD C	RA	U	LG	IC TH	1	361	HA	v	10	R	C F	GCH	R

```
THEN: COMPUTE LIQUEFIED MATERIAL MOVEMENT [FGMELT]
       :ENDIF:
       : IF: REGION BOUNDARY IS DISRUPTED?
       : THEN:
              SET DISRUPTION - LAS
              :SET N TO I+1
              SET T(N) TO CURRENT TIME
       :ELSE:
              ESTIMATE TIME FOR BOUNDARY DISRUPTION [FGESTT]
              :IF: ESTIMATED TIME IS .LT. T(I+2), :THEN: T(I+2)=EST. TIME
0000000000000
       :ENDIF:
   :ENDO:
                                          (41), BEDTMP (41), COLTMP (41),
(41), ROMX (40), CPMX (40),
(40), XKMX (40), TC (20),
                                EL VAY
         DIMENSION
        +
        +
        +
cc
                           ROZR
XMUCD
SURTC
ROSAT
XKMX
                                         ROZRO2
ROCOL
CPCOL
TMELT
XMUF3
                                                       ROUO2
XMUCOL
XKCOL
XLATC
RODEB
                                                                    ROSTR
ROVAP
XKVAP
ROMX
                                                                                  RCABS
XMUVAP
CPDEB
CPMX
                                                                                                ROCOLD ,
HEG ,
TSAT ,
XMUX ,
                                                                                            , , , ,
         COMMON
                                      ,,,
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        +
        +
        ++
                                      ,
                                                                  ,
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00 0000 00
                            DISRUP
         LOGICAL
         NSTPC = 10
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```
CALL FRIIME TO BREAKUP TIME STEP COMING FROM DBUNDL INTO SMALLER INTERVALS WHICH WILL DEPEND ON THE VALUE OF NSTP
000
         CALL FRTIME ( T (I) , DELTT , TC , NSTPC )
C
         J = 1
C
    10 CONTINUE
000
   TEST TIME TO PREVENT ENTERING TIME FROM BEING ZERO
         IF
              ( TC( J ) .EQ. 0.0 )
                                               J = J + 1
C
        IF
             ( J .LT. NSTPC ) THEN
C
              CURTIM = TC ( J )
DELTC = TC ( J + 1 ) - TC ( J )
000
                                                      , ZROZMC ,
HITEC ,
PDROPC ,
                             ( XMASSC , ZRMC
        CALL
               FRCHAR
                                                                                    S TRMC
VINCOD
KTERMC
                                                                   , UD2MC
                                                                                 ,
                                ABSIC
                                             AREAR ,
POROSC ;
                                                                      VINC
       +
                                         ,
                                                                                 ,
                                                                                              ,
       4
                                          3
0000
   CALL FROZTH TO DETERMINE THE BEHAVIOR OF POROUS BED
                               EFFDIA
ZROZTC
HTLBCD
MAXL
BEDTMP
FISHC
DOWNZ
                                             POR OSC
ZROZAC
HTLBCC
DELTC
COLTMP
HYDGC
DISRUP
                                                          HITEC
ALPHTC
HTUBCD
IDREGN
THMUTC
FGRSC
                                                                       YCHRL
ALPHAC
HTUBCC
NOND
ELVMC
VOLGSC
                                                                                    VINC
ELVNC
ND
ELVAY
OXDAC
IMT
         CALL
                 FROZTH
                             (
                                                                    ,
                                         ,
                                                       ,
                                                                                 ,
                                                                                               ,
                                         ,
       +
                                                       ,
        ٠
                                                       ,
                                                                    ,
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       +
                                          ,,
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       ٠
                                                       ,
                                                                    ,
                                                                                 ,
                                                                                               .
                                          ,
                                                                    ,
                                                       3
                                                                                 .
0000
   COMPUTE LIQUIFIED MATERIAL MOVEMENT IF DEBRIS BED MELTING OCCURS
                       FRMELT
                                     NOND , IMT
                                                             , ELVMC , ELVAY , DELTC ,
              CALL
                                   (
00000000
   CHECK FOR LOWER REGION BOUNDARY BREAKTHROUGH
   IF BREAKTHROUGH OCCURS, RETURN TO DBUNDL WITH END OF TIME INTERVAL
              IF ( DISRUP ) THEN
C
                    NSTPC . J
C
              ELSE
```

```
C
                      CALL FRESTT ( ELVMC , ELVNC , VELMTC , CURTIM ,
0000
   IF ESTIMATED TIME OF BREAKTHROUGH IS GREATER THAN CURRENT TIME
PLUS ADJUSTED DELTA TIME, SET CURRENT TIME TO NEXT TIME INTERVAL
                       IF ( ESTDT .GT. TC( J + 1 )) THEN
С
                             CURTIM . TC( J + 1 )
Ç
                       ELSE
00000
   IF ESTIMATED TIME OF BREAKTHROUGH IS LESS THAN CURRENT TIME PLUS
ADJUSTED DELTA T, SET CURRENT TIME TO ESTIMATED TIME AND NEXT TIME
INTERVAL TO CURRENT TIME
                             CURTIM . ESTDT
TC( J + 1 ) . CURTIM
C
                       ENDIF
000
                ENDIF
0000
   WHEN J IS GREATER THAN NSTPC, CONTROL WILL RETURN TO DBUNDL WITH CTIMEC CONTAINING THE CURRENT TIME FOR CURRENT REGION
                G0 T0 10
C
          ENDIF
С
          RETURN
CC
          END
```

TABLE A-2. LISTING OF FRTIME

```
00
          SUBROUTINE FRTIME ( TIMIN , DELTT , TC , NSTP )
SUBCODE NAME: FRIME
PURPOSE: TO DEFINE THE COHESIVE DEBRIS TIME STEP
CALLING SUBROUTINES: DBFROZ
SUBROUTINES CALLES: NONE
WORKPACKAGE: 15
ENGINEER/PROGRAMMER: S.T.HSIEH/G.H.BEERS
LANT MODIFICATION DATE: 11/30/81
   INPUT VARIABLES
                                                                   DESCRIPTION
                                  TIME STEP CALCULATED IN THE DISRUPTED BUNDLE TIME
STEP SUBROUTINE DETIME
NUMBER OF STEPS IN WHICH TIME STEP FROM DETIME WILL
BE BROKEN
        DELTIN
        NSTP
                                                                   DESCRIPTION
   GUTPUT VARIABLES
                                  TIME STEP TO BE USED IN COHESSIVE DEBRIS ANALYSIS WH
IS DERIVED FROM DISRUPTED BUNDLE ANALYSIS TIME STEP
        DELTOT
                            TC ( NSTP + 1 )
          DIMENSION
CC
          STEPS . DELTT / FLOAT ( NSTP )
C
          DO 10 I . . . NSTP + 1
C
                 TC ( I ) * TIMIN + FLOAT ( I + 1 ) * STEPS
C
     10 CONTINUE
C
          RETURN
          END
```

TABLE A-3. LISTING OF FRCHAR

SUBROUTIN 1 AREAR, HI 2 POROSC, PI	E FRCHAR(XMASSC, ZRMC, ZRO2MC, UO2MC, STRMC, ABSMC, TEC, VINC, VINCOD, DELTC, DROPC, YCHRL, KTERMC, EFFDIA)
PURPOSE	TO DEFINE COHESIVE BED CHARACTERISTICS AND
CALLING	SUBROUTINE: DBFROZ
SUBROUTIN	NE CALLED: NONE
ENGINEER	PROGRAMMER: STH
LAST DAT	E MODIFIED: 8/10/81
INPUT VAL	RIABLES:
XM ASSC	TOTAL MASS OF DEBRIS ACCUMULATED FOR ALL COMPONENTS(KG)
ZRMC	TOTAL MASS OF ZR ACCUMULATED FOR ALL COMPONENTS (KG)
ZRO2MC	TATAL MASS OF ZROZ ACCUMULATED FOR ALL COMPONENTS(KG)
UD2MC	TOTAL MASS OF UD2 ACCUMULATED FOR ALL COMPONENTS(KG)
STRMC	TOTAL MASS OF CORE STRUCTURAL MATERIALS
ABSMC	TOTAL MASS OF CONTROL ROD MATERIAL ACCUMULATED (KG)
AREAR	TOTAL BUNDLE CROSS SECTIONAL AREA(M2)
HITEC	FROZEN DEBRIS REGION HEIGHT FROM DBREGN(M)
VINC	CODLANT VELOCITY AT INLET OF COHESIVE DEBRIS REGION(M/SEC)
VINCOD	COOLANT INLET VELOCITY AT PREVIOUS TIME STE (M/SEC)
DELTC	TIME STEP (SEC)

OUTPUT VARIABLES: POROSC BED POROSITY PRESSURE DROP ACROSS THE BED(PA) PDROPC CHARACTERISTIC LENGTH OF FROZEN BED, DERIVED FROM PRESSURE DROP EQUATION, M YCHRL FLAG, =0 NORMAL RUN, =1 ABNORMAL TERMINATION KTERMC EFFECTIVE PARTICLE DIAMETER DERIVED FROM SPECIFIC SURFACE AREA (M) EFFDIA AT THIS TIME, ALL MATERIALS PROPERTIES ARE ASSUMED COMING THROUGH COMMON BLOCK, THESE INCLUDE: ROZR ZR DENSITY(KG/M3) ROZRO2 ZRO2 DENSITY (KG/M3) RGU02 UD2 DENSITY (KG/M3) ROSTR DENSITY OF STRUCTURAL MATERIAL (KG/M3) DENSITY OF CONTRAL ROD MATERIAL(KG/M3) ROABS COOLANT DENSITY(KG/M3) ROCOL VISCOSITY OF COOLANT (KG/SEC/M) X MUC OL ROZR XMUCD SURTC ROSAT XKMX ROZRO2 ROCOL CPCOL TMELT XMUF 3 ROUO2 XMUCOL XKCOL XLATC RODEB RDABS XMUVAP CPDEB CPMX ROCOLD HEG TSAT XMUX R DS TR R DV A P XK V A P R DM X COMMON ,,, , , , , ,,, , , ,,, , + , , , ,, , + , . , 4 , 0000 CALCULATE AVERAGE BED POROSITY POROSC +0 - (ZRMC / ROZR + ZRO2MC / ROZRO2 + UO2MC / ROUD2 + STRMC / ROSTR + ABSMC / ROABS) / (AREAR * HITEC) . 1 ĉ CHECK POROSITY

C IF (POROSC .GT. 1.00 .OR. POROSC .LT. 0.00) THEN KTERMC = 1 WRITE (6 , 100) ¢ ELSE 00000 SET SPECIFIC SURFACE AREA OF POROUS BODY=SURFACE EXPOSED TO THE FLUID PER UNIT VOLUME OF SOLID. FROM A. E. SCHEIDEGGER, 3RD EDITION, P16, SPSUF=8.0E5(1/M) SPSUF = 8.0E+05 EFFDIA = 6.0 / SPSUF ¢ CALCULATE PRESSURE DROP ACROSS COHESIVE DEBRIS BED č XITM1 = (VINC - VINCOD) * ROCOL / DELTC ALPHA = 150. * (1.0 - POROSC) ** 2 / (AMAX1(POROSC,1.0E-8)) ** 3 / (EFFDIA ** 2) BETA = 1.75 * (1.0 - POROSC) / (AMAX1(POROSC,1.0E-8)) ** 3 / EFFDIA PDROPC = XITM1 + (ALPHA * XMUCOL + BETA * ROCOL * VINC) * VINC PDROPC = PDROPC * HITEC KTERMC = 0 YCHRL = BETA / (AMAX1(ALPHA , 1.0E-6)) 1 1 + C ENDIF C 100 FORMAT(2X, 78HMASS CALDULATION IS WRONG; BED POROSITY IS EITHER NEG LATIVE OR GREATER THAN ONE) C RETURN

TABLE A-4. LISTING OF FROZTH

SUBROUTINE	FROZTH	C EFFDID ZRDJCC HTLBCC MAXL BEDTMI FISHC DDWNZ	A , PORDSC C , ZROZACC HTLBCC D ELTT P , CDLTMP , HYDGC , DISRUP	HITEC ALTHECD HICREGN HICREGN FGRSC	YCHRL , VINC , ALPHAC , ELVNC , HTUBCC , ND , NOND , ELVAY , ELVMC , OXDAC , VOLGSC , IMT
PURPOSE: T BED.	O CALCULA	TE THERM	ALLY RELAT	ED BEHAVIORS	S OF A POROUS
CALLING SU	BROUTINES	DBFROZ			
SUBROUTINE	CALLED	TEMPSR			
ENGINEER/P	ROGRAMMER	:STH			
LAST DATE	MODIFIED:	8/10/81			
INPUT VARI	ABLES:				
EFFDIA	EFFECTIVE	PARTICL	E DIAMETER	OF A PORCUS	BODY(M)
POROSC	DEBRIS BE	D POROSI	TY		
HITEC	BED HEIGH	T (M)			
YCHEL	CHARACTER	ISTIC LE	NGTHEF PER	CUS BODY FR	DM DELT P, M
VINC	COOLANT I	NLET VEL	OCITY (M/SE	C)	
ZROZTC	EFFECTIVE	ZRO2 RE	ACTION LAY	ER THICKNES	S (M)
ZROZAC	EFFECTIVE	ZR-STEA	M REACTION	AREA(M2)	
ALPHTC	EFFECTIVE	ALPHA-Z	R REACTION	LAYER THIC	KNESS.M
ALPHAC	EFFECTIVE	ALPHA-Z	R REACTION	AREA (M2)	
ELVNC.	EL EVATION	OF PORD	US BODY-FR POROUS BOD	OM THE BOTT	OM OF ROD BUNDLE
HTLBCD	HEAT TRAN	SFER INT	O DEBRIS E	ED AT LOWER	BOUNDARY, W/M2
HTLBCC	HEAT TRAN	SFER INT	O COOLANT	AT LOWER BO	UNDARY, W/M2
HTUBCD	HEAT TRAN	SFER INT	O DEBRIS B	ED AT UPPER	BOUNDARY / M2
HTUBCC	HEAT TRAN	SFER INT	O COOLANT	AT UPPER BO	UNDARY, W/ M2
HTUBCC	HEAT TRAN	SFER INT	O COOLANT	AT UPPER BO	UNDARY, W/ M2

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	ND	NUMBER OF NODES TO BE USED IN LITCUID OF VARON PEGIDA
** **	MAYI	HUNDER OF HODES TO BE USED IN EIGOID OR VAFOR RESIGN
**	HAAL	COMBINED LIQUID, SATURATION AND VAPOR REGION,
	DELTT	TIME STEP(S)
	INPUT/OU'	TPUT VARIABLES:
	IDR EGN	REGION TYPE I.D. =1 VINC GT O ONE LIQUID REGION =2 VINC GT O ONE VAPOR GEGION =3 VINC GT O OND SAT. REGION =4 VINC GT O TWO REGIL & S =5 VINC GT O TWO REGIS & V
		= 6 VINC GT O THREE REG LESEV = 7 VINC=C DNE LICUID REG
	NOND	=0 VINC=0 UNE VAPUK REG
* 36 36 36 36	NUND	NUMBER OF NEUES USED IN POROUS BODT ANALTSIS, ND IDREGN=1,2,7,8 =3 IDREGN=3 =ND+2 IDREGN=4,5 =2*ND+1 IDREGN=6
	ELVAY	ELEVATION OF NODES IN DEBRIS, ELVAY(1)=ELVNC ELVAY(NOND)=ELVNC+HITEC
	BEDTMP	DEBRIS TEMPERATURE CORRESPONDING TO NOND NODES
	COLTMP	CODLANT TEMPERATURE CORRESPONDING TO NOND NODES
	DXDAC	ZR-STEAM HEAT GENERATION RATE(W/M3)
34.34	FISHC	FISSION/DECAY HEAT GENERATION RATE(W/M3)
XXX	DUTPUT V	ARIABLES:
	THMOTC	MOLTEN MATERIAL THICKNESS(M)
ŝ	ELVMC	MOLTEN CORE REGION ELEVATION AT LOWER BOUNDARY, M
č	HYDGC	HYDROGEN GENERATION DURING DELTT(MOLES)
č	FGRSC	FISSION GAS RELEASE(MOLES) DURING DELTT
31 31	VOLGSC	VOLATILE FISSION PRODUCTS RELEASE DURING DELTT, MOLE
i co	IMT	DEBRIS REGION TYPE, =0 SOLID REGION, =1 MOLTEN REGION TOTAL OF NOND VALUES

DOWNZ	LENGTH OF MOLTEN POOL PENETRATION, M
	AFTER CURRENT TIME, S
DISRUP	DISRUPTION FLAG
AT THIS THROUGH	TIME, ALL MATERIALS PROPERTIES ARE ASSUMED COMING COMMON BLOCK, THESE INCLUDE:
ROCOL	LIQUID CODLANT DENSITY(KG/M3)
ROVAP	STEAM DENSITY(KG/M3)
XMUCOL	LIQUID CODLANT VISCOSITY(KG/SEC/M)
XMUVAP	VAPOR VISCOSITY(KG/SEC/M)
HFG	LATENT HEAT OF VAPORIZATION (J/KG) OF COULANT
SURTC	SURFACE TENSION OF COOLANT(PA)
CPCOL	LIQUID SPECIFIC HEAT(J/K/KG)
XKCOL	LIQUID COOLANT THERMAL CONDUCTIVITY)W/M/K)
XKVAP	VAPOR(STEAM) THERMAL CONDUCTIVITY(W/M/K)
CPDEB	SPECIFIC HEAT OF DEBRIS(J/K/KG)
ROZR	ZR DENSITY(KG/M3)
RCZR02	ZRO2 DENSITY(KG/M3)
ROUC2	LO2 DENSITY (KG/M3)
ROSTR	DENSITY OF STRUCTURAL MATERIAL(KG/M3)
ROABS	DENSITY OF CONTROL ROD MATERIAL (KG/M3)
XMUDEB	VISCOSITY OF DEBRIS(KG/SEC/M)
XKDEB	THERMAL CONDUCTIVITY OF DEBRIS (W/M/K)
TSAT	SATURATION TEMPERATURE OF COOLANT OF FROZEN DEBRIS

```
WATER DENSITY AT SATURATION(KG/M3)
          RCS AT
0000000000
         TMELT
                          MELTING TEMPERATURE OF DEBRIS MATERIAL(K)
                          LATENT HEAT OF FUSION FOR DEBRIS MATERIAL(J/KG)
          XLATC
                                                 BEDIMP(41)
COLTMO(41)
XKMX(40)
TCOLT(20)
                                                                      COLTMP(41) ,
ROMX(40) ,
TEMPBO(20) ,
                                                                                           IMT(41)
CPMX(40)
TEMPB(20)
                            ELVAY(41) ,
BEDTMG(41) ,
XMUX(40) ,
TCOLTU(20) ,
          DIMENSION
                                                                  ;
                                                                                       ;
        +
                                                                   ,
CC
                             ROZR
XMU:D
SURTC
ROSAT
XKMX
                                           ROZRO2 ,
CPCOL ,
TMELT ,
XMUF3 ,
                                                         ROUO2
XHUCJC
XKCOL
XLATC
RODEB
                                                                                      RGABS
(HJ/AP
CPDEB
CPMX
                                                                                                    ROCOLD ,
HFG ,
TSAT ,
XMUX ,
                                                                        ROSTR
RJV AP
XKVAP
ROMX
                                                                                                 ,
         COMMON
                                                                                   ,,,
                                                                    ;
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        +
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        +
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                                                                                   .
                                                                                                  ,
        +
                                        .
cc
          LOG ICAL
                             DISRUP
0000 000
                      PI / 3.14159 /
          DATA
   CALCULATE VOLUMETRIC HEAT GENERATION RATE QVOL (W/M3)
          AVOL = DXDAC + FISHC
C
          ELVOD . ELVMC
0000
   BASED ON QVOL, VINC, AND COLTMP CHECK THE REGION ID
  2020 CONTINUE
CC
                         100.0
          XLL IQ
XLSAT
XLVAP
                   ::
CCC
   CALCULATE DRYOUT HEAT BASED ON LIPINSKI'S 1-D MODEL
        CALL DRYCUT(VINC, PORDSC, HITEC, EFFDIA, PDROPC, GVCL, ROCOL, ROVAP,
+XMUCDL, XMUVAP, HFG, SURTC, QDYCUT)
CC
          IF ( VINC .LE.
                                                  THEN
                                   0.0)
C
```

```
COMPARE QVOL TO QDYOUT
ç
                   ( OVOL * HITEC * (1.0 - PORDSC) .GE. QCYOUT ) THEN
              IF
C
             ELSE IDR . 7
ç
             ENDIF
¢
        ELSE
000
   REGION TYPE 1-6 LEFT TO BE IDENTIFIED
                  ( COLTMP(1) .GT. TSAT ) THEN
              IF
C
             ELSEIF
                         ( COLTMP(1) .EQ. TSAT )
IF ( COLTMP(NOND) .EQ. TSAT )
IDR - 3
                                                                       THEN
C
                         ELSE
000
  CALCULATE SATURATION REGION LENGTH
                              XLSAT - ROCOL * VINC * HEG / CVOL / . I.E-8 )
AMAX1 (( 1.0 - PDROSC ) , 1.E-8 )
       4
                              IDR = 5
XLVAP = HITEC - XLSAT
C
                                  ( QVOL * HITEC * ( 1.0 - POROSC )
.LT. COYOUT ) IDR = 3
                              IF
C
                              IF ( KLSAT .GE. HITEC ) IDR = 3
IF ( COLTMP(NOND) .LT. TSAT ) IDR = 3
C
                         ENDIF
C
                   ELSE
000
   COLTMP(1)
                  .LT. TSAT
                         IF ( COLTMP(NOND) .LT. TSAT ) THEN
C
                         EL SE
                              XLSAT - ROCOL * VINC * HFG / GVOL /
AMAX1 (( 1.0 - POROSC ) , 1.E-8 )
XLLIQ - XLSAT/HFG * CPCOL * (TSAT - COLTMP(1))
       ٠
C
                              IF ( COLTMP(NOND) .EQ. TSAT )
                                                                           THEN
```

```
IDR = 4
XLSAT = HITEC - XLLIG
C
                                                    IF ( XLSAT .LE. 0 )
                                                                                                  IDR = 1
Ċ
                                           ELSE

IDR = 6

XLVAP = HITEC - XLLIQ - XLSAT

IF (QVOL + (HITEC - XLLIQ) + (1.0 - POROSC)

IF (QVOL + (HITEC - XLLIQ) + (1.0 - POROSC)
          +
C
                                                    ELSE
                                                            IF ( (XLLIQ + XLSAT) .GE. HITEC ) THEN
IDR = 4
XLSAT = HITEC - XLLIQ
IF ( XLLIQ .GE. HITEC ) IDR = 1
C
                                                            ENDIF
C
                                                   ENDIF
Ċ
                                           ENDIF
C
                                   ENDIF
C
                           ENDIF
C
                    ENDIF
C
            ENDIF
0000000
   DEBRIS REGION TYPE HAS BEEN IDENTIFIED, IDR=1-8, IF IDR AND
IDREGN ARE NOT CONSISTANT, CALL SUBROUTINE REGMOD TO ADJUST
TEMPERATURE OF BED AND COOLANT, NODES ELEVATION AND SET IDREGN
EQUAL TO IDR
          CALL REGMOD(IDR, MAXL, ND, IDREGN, NOND, XLLIG, XLSAT, XLVAP,
+ELVNC, TSAT, HITEC, ELVAY, BEDTMP, COLTMP)
C
            N2 . ND . 2
C
            DO 50 I = 1 , NOND
C
                    BEDTMO(I) - BEDTMP(I)
COLTMO(I) - COLTMP(I)
C
      50 CONTINUE
COC
    BASED ON COLTMP AND BEDTMP, ROMX(N2), CPMX(N2), XMUX(N2) AND
XKMX(N2) ARE KNOWN ASSUME THEY ARE TEMPERATURE DEPENDENT,
```

```
FIRST N VALUES ARE FOR BED AND THE REST N VALUES ARE FOR CODLANT.
0000000
   NOW CALCULATE TEMPERATUR OF BED AND COOLANT FOR CURRENT TIME
          IF ( IDREGN .EQ. 1 .OR. IDREGN .EQ. 2 )
                                                                                   THEN
C
                         ( IDREGN .EQ. 1 )

. IDREGN .EQ. 2 )

. 0.0

. 0.0

. 0.0

. 0.0

. 0.0
                 IF
VAR1
VAR2
VAR3
VAR4
                                                         IDYOT -0
                        (
0000
                 CALL MATPRO ( BEDIMO , COLIMO , ND , N2 , ROMX , CPMX , XKMX , XMUX , IDREGN ; IDYOT )
                  DO
                        100
                                 I = ND + 1 , N2
C
                        VAR2
VAR2
VAR3
VAR4
                                VAR1
VAR2
VAR3
VAR3
                                            + CPMX(1)
+ XKMX(1)
+ XMUX(1)
                                                               / FLOAT (ND)
                                                              1
                                                                  FLOAT (ND)
Ç
                 CONT INUE
    100
CC
                 XRENC = VAR1 * VINC * YCHRL / VAR4
XPRD L =VAR2 * VAR4 / VAR3
C
                               7. - ( 10. - 5. * POROSC ) * PORCSC ) *

1. * .7 * XRENO ** .2 * XPRDL ** ( 1. /

1. 33 - ( 2.4 - 1.2 * POROSC ) * POROSC )

** .7 * XPRDL ** ( 1. / 3. )
                  XNU
                       .
                            1
                                                                                                   3 . )) +
) * XREND
         +
         +
         +
C
                  HVSC = XNU + VAR3 / YCHRL ++ 2
CC
                  DELTZ . HITEC / FLOAT( ND-1 )
C
                 ( IDYDT .EQ. 1 ) THEN
HVSC = (YCHRL * ( 1.0 - POROSC ) / .00377) ** 1.33
* XREND ** 0.65 * VAR3 / YCHRL ** 2
          IF
         +
C
          ENDIF
C
                                                             N2
HTLBCD ; HTLBCC ; HTUBCD ; HTUBCC ;
VINC ; VOL ; DELTT ; DELTZ ;
                                             ND
HVSC
POROSC
BEDT MP
                  CALL
                            TEMPSR
                                          (
                                                          ,,,
         +
         +
         4
C
                         ( IDREGN .EQ. 1 )
                                                           THEN
                  IF
```

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```
DO 150 I . 1, NOND
CONTINUE (COLTMPII) .GE. TSAT) COLTMPII) - TSAT
  150
C
                  ELSE IF ( IDREGN .EQ. 2 ) THEN
DO 160 I = 1 , NOND
IF ( COLTMP(I) .GE. TSAT) COLTMP(I) = TSAT
CONTINUE
   160
C
                  ENDIF
CC
           ELSE IF (IDREGN.EQ.7.DR.IDREGN.EQ.8) THEN
XNU = 7.0 - ( 10.0 - 5.0 * POROSC ) * POROSC
C
                  IF { IDREGN : EQ: 3 } IDYOT : 1
C
                  VAR1 = 0.0
000
                   CALL MATPRO ( BEOTMO , COLTMO , ... , ...
                  DO 200 I * ND + 1 N2
VARI * VARI + XKMX(I) / FLOAT(ND)
CONTINUE
   200
Ċ
                  HVSC = XNU * VAR1 / YCHRL ** 2
DELTZ = HITEC / FLOAT( ND - 1)
C
                         ( 1DYOT .EQ. 1 ) THEN
HVSC * (YCHRL * ( 1.0 - POROSC) / .00377) ** 1.33
* XRENO ** .65 * VAR3 / YCHRL ** 2
                  IF
         +
C
                  ENDIF
C
                                          ( ND , N2 , IDYOT , BEDING , COLING ,
HVSC , HILBCD , HILBCC , HIUBCD , HIUBCC ,
POROSC , VINC , OVOL , DELIT , DELIZ ,
BEDIMP , COLIMP )
                  CALL TEMPSR
         ++
         +
CC
                         ( IDREGN .EQ. 7 ) THEN
DO 201 I . 1, NOND
IF ( COLTMP(I) .GE. TSAT ) COLTMP(I) - TSAT
CONTINUE
                  IF
   201
C
                  ENDIF
UUUUUUU
   IF IDREGN EQUALS TO 3, QVOL IS USED TO HEAT SATURATED WATER
NO BED AND CODLANT TEMPERATURE CHANGES ASSUMED, I.E. NO
CALCULATION OF TEMPERATURE IS NEEDED
```

C

	ELS	E I	F		(]	0	RE	6	Ν.	E	Q	• •	•)			T	н	EN																							
		IDY	1	ľ	:	0×	LL	. 1	9	1	1	FL	.0	A	T	t	N	D	-		L)																			
		VAR	1234		0000		0000																																		
		CAL	. L		MA	T	PF	20	1	(B	E (T	M	0	,	1	cc	L	T	MC)	,		•	•	,	į	•••	•											
		00		30	0		I		1	ND	6. 1	•	1		,	N	2																								
				VANAN	RARR	1234	:	SX XX	-	1234		++++	RUXX	OP XX	MM M	(((((((((((((((((((ILLI	>>>>>>>>>>>>>>>>>>>>>>>>>>>>>>>>>>>>>>>	1111	-		0000	AAAA		22.22																
00		COM	T	IN	U	Ē																																			
		XRE	NO	2	:	v	A	R1 R2		:	¥	I	1024		*	Y	CA	HR.	L	1	1	۷	4	24																	
:		XNU	J	•	() *)	7.0	ORN		10	•••	017		5.	Swo	*		R ;*	05 + 1 ()	11	0	*P3		RUO	35.	C4	2	*(12	• P	¢	RO	74	X	RE *P	NI	R	*()S	2:2			
		HVS	sc			XN	U			44	R	3	1		Y	C +	R	L	*	*	-	2																			
		DO		40	0	PA	I		,	1.	,	a	ND	Т	MI	1	T	1																							
00		co	NT	İC		Ē	ŏ	ÌÌ)	•		či	δĭ	Ť	MI	i č	Î	j																							
	:	CA	LL	1	E	MF	s	R		(ZIOT	DVOE	SCREP	is a	C	,,,,		NHVI		BCL	C C T)	,,,,	HEC	DIT	LI	BC	c	,,,		HT	MI L	BC	00	, , ,				•••		
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```
¢
              IF( (BEDIMP(I)+BEDIMP(I+1))/2.0 .GT. INELT ) THEN
000
        TMELT IS DEBRIS BED MELTING TEMPERATURE FROM MAPRO
                    IMG - IMG + 1
JUP - I + 1
IMT(I) - 1
C
              ELSE
                    ISG . ISS . 1
IMT(I) . 0
C
              ENDIF
C
 2000 CONTINUE
cc
         00
             2010 I . 1 , NOND - 1
C
              J = NOND - I
DTMP1 = ( BEDTMP(J+1)+BEDTMP(J) ) / 2.0 - THELT
C
              IF ( DTMP1 .LT. 0.0 )
CTMP1 = 0.0
                                                THEN
Ċ
              ELSE
DOWN Z=DOWNZ+DTMP1*(ELVAY(J+1)-ELVAY(J))*CPDEB/XLATC
BEDTMP(J+1) = TMELT
BEDTMP(J) = TMELT
C
              ENDIF
C
                                      GO TO 2010
              IF ( J .EQ. 1 )
¢
              IF ( IMT(J) .GT. IMT( J-1 ) ) THEN
000
         MOLTEN MATERIALS MELTING THE LOWER NODE
                    IF (DOWNZ GT. (0.5*(ELVAY(J)-ELVAY(J-1))) THEN

BEDTMP(J) = TMELT

BEDTMP(J-1) = TMELT

IMT(J-1) = 1

DOWNZ = DOWNZ - ( ELVAY(J) - ELVAY(J-1) )
C
                    ENDIF
C
              ENDIF
CC
  2010 CONTINUE
THMOTC . 0.0
C
```

```
IF ( IMT (1) .EQ. 1 ) THEN
THMOTE - THMOTE + 0.5 + ( ELVAY (2) - ELVAY (1))
000
   SET DISRUPTION FLAG WHEN DEBRIS REGION TYPE = 1, INDICATING MELTING
               DISRUP . .TRUE.
С
         ENDIF
C
              ( IMT (NOND) .EQ. 1 ) THEN
THMOTE - THMOTE + 0.5 + ( ELVAY (NOND) - ELVAY (NOND - 1))
         IF
C
         ENDIF
C
             3020 I = 2 , NOND - 1
         DO
C
                   ( IMT (I) .EQ. 1 ) THEN
THMOTC = THMOTC + 0.5 * ( ELVAY (I + 1) - ELVAY (I - 1))
               IF
C
               ENDIF
C
  3020 CONTINUE
C
00000000
        NOW ADJUSTED BED TEMPERATURE AND MELTEN REGION HAS BEEN DEFINED
       CALL CHEMHT(ZROZTC, ZROZAC, ALPHTC, ALPHAC, IDREGN, NOND, BEDTMP,
COLTMP, ELVAY, DELIT, OXDAC, HYDGC)
CALL NUCLHT(IDREGN, NOND, BEDTMP, ELVAY, DELIT, TOTIME, ... ETC)
         QVOLN = OXDAC + FISHC
C
 IF ( IITMP .GT. 50 ) THEN
WRITE ( 2050 )
2050 FORMAT(2X, 57HITERATION MORE THAN 50 TIMES NO CONVERGENCE IN TEMP.
(AL.)
GO TO 2030
C
        ENDIF
C
        IF ( ABS((OVOLN-OVOL)/QVOLN) .GT. 0.05 ) THEN
C
        ENDIF
 2030 RETURN
```

TABLE A-5. LISTING OF FRMELT

```
CC
        SUBROUTINE FRMELT ( NOND , IMT , ELVMC , ELVAY , DELTC ,
SUBCODE NAME: FRMELT

PURGPOSE: TO MEASURE THE LIQUID MATERIAL MOVEMENT WHEN GEBRIS BED

MELTING OCCURS.

CALLING SUBROUTINES: DBFROZ

SUBROUTINES CALLED: NONE

WORK PACKAGE: 15

ENGINEER/PROGRAMMER: S.T.HSIEH/G.H.BEERS

LAST MCDIFICATION DATE: 11/30/81
                                      DESCRIPTION
NUMBER OF NODES USED IN PORDUS BODY ANALYSIS
DEBRIS REGION TYPE: = 0, SOLID REGION
= 1; MOLTEN REGION
MOLTEN CORE REGION ELEVATION AT LOWER BOUNDARY
ELEVATION OF NODES IN DEBRIS
   INPUT VARIABLES
          ELVMC
ELVAY
DELTC
   OUTPUT VARIABLES
                                       VELOCITY OF MOLTON POOL FLOWING DOWNWARD (M/S)
          DIMENSION
                               ELVAY( NOND ) , INT( NOND )
0000
   SAVE INCOMING ELEVATION OF MOLTON MATERIAL
          ELVMO . ELVMC
C
   DO 100 (I .1 , NOND
IF (IMT(I) .EQ. 1 )
                                                          GO
                                                                 TO
                                                                       110
C
   110 IF ( I .LE. NOND )
                                               ELVMC = ELVAY(I)
C
          VELMTC = AMAX1( 0.0 , (ELVMO - ELVMC)) / DELTC
C
          RETURN
```

TABLE A-6. LISTING OF FRESTT

SUBROUTINE FRESTT (ELVMC , ELVNC , VELMTC , CURTIM , ESTDT) SUBROUTINE FRESTT THE TIME OF DISRUPTION CALLING SUBROUTINES: DBFRAG SUBROUTINES CALLED: NONE CALLING SUBROUTINES: DBFRAG SUBROUTINES CALLED: NONE WORK PACKAGE: 15 C ENGINEER/PROGRAMMER: S.T.HSIEF/G.H.BEERS LAST MODIFICATION DATE: 11/30/31 INPUT VARIABLES ELVMC ELVNC ELEVATION OF RUBBLE BODY FROM THE BOUNDARY ELVNC ELEVATION OF RUBBLE BODY FROM THE BOTTOM OF ROD BUNDLE TO BOTTOM OF RUBBLE BODY REGION (M) VELMIC VELOCITY OF MOLTEN POOL FLOWING DOWNWARD (M/S) CURTIM CURRENT TIME (S) OUTPUT VARIABLES ESTIMATED TIME OF DISRUPTION (S) TESTCC = ABS(ELVMC = ELVNC) / AMAX1(1.0E-08 , VELMTC) ESTOT = CURTIM + TESTCC RETURN

	\$	U	B	20		T	I	N	E			DE	3 F		2 A	G			ť	UN ANY THE YO	ITILORLOEI	NRXY TYRUS	ATRZ TOTA	VR R RPCU	R		,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	NANH NACOTO	XAZHALDO L	HARTA LAL	ASPZELAAR T	SRTR RRL	RRD		,,,,,,,,,,,,		ZARTECIE		RAZBETHU	RARTMRIT	RCRD	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,		ZHAHIBHKI	TOPUTE	2R HBETER	MGHRGERE	RRDRR	,,,,,,,,,		VAHNTPD		MAHBROOM	R DAR	ONC RN	,,,,,,,,
SUBRUR SU	COLAKIT	DUNZDOWZ	EEGTACE	N SNK/I	UEAPE	ERBNGRH	EUR EUC	BOCIGA	BUART	LTLAI	DEILIMO	E NESKN			R	F	SDG S:	BI		HANDAR	11, 15/	Y F IN	S R HO	I A H/	S G /8	G	DR H	1.		88	R	R	S																							
DBFI KEE VAR	RRPIT	GTOL	ARL	AEOSL	S X M	N DB	BUCCIE	ELER	HICK H	ZUDZO	GISF	MIMI				EIO	LIZZZ	EINN		I	ROLLE	mz D R M	SSRA .	PG	0S*	NINN					TH	HE	E	AN	NSI	ESV AL		SAFFL	TES	G I T	FOFA	TIN	HHAN	ESL.	TFAR	BHOR	UARA	NC T My	DL0	BI	E		I	0.	IN	G
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	: C	0	M	PL	T	E		D	E	B	R	I	s	-	BE	0		T :-	4 5	R	M	4	L	L	Y	_	2 1	FL		1	TE	- 0	1	8	FI	H	4.4	11	10	R		ſ	F	RI	TH	R	-	1								

TABLE A-7. LISTING OF DBFRAG

```
#IF: DEBRIS BED MELTING OCCURS?
             :THEN: COMPUTE LIQUEFIED MATERIAL MOVEMENT
       :ENDIF:
       :IF: REGION BOUNDARY IS DISRUPTED?
       ITHENI
             SET DISRUPTION FLAG
             :SET N TO I+1
             SET T(N) TO CURRENT TIME
        IELSE:
             ESTIMATE TIME FOR BOUNDARY DISRUPTION [FREST]
             :IF: ESTIMATED TIME IS .LT. T(I+2), :THEN: T(I+2)=EST. TIME
        :ENDIF:
  :ENDO:
         IMPLICIT INTEGER ( I - N )
                                           41102
        DIMENSION
                               ELVAR
IRT
XMUX
                                                   , BEDTMR ( 41 ) , CULTMR ( 41 ) ,
RUMX ( 40 ) , CPMX ( 40 ) ,
XKMX ( 40 ) , TR ( 20 ) ,
                                         ((
       +
       +
       ٠
CC
                          ROZE
XMUCD
SURTC
ROSAT
XKMX
                                       ROZRO2
ROCOL
CPCOL
TMELT
XMUF 3
        COMMON
                                                    ROUD2 , ROSTR
XMUCOL , ROVAP
XKCOL , XKVAP
XLATC , ROMX
RODEB
                                                                               ROABS , ROCOLD ,
XMUVAP , HFG ,
CPDEB , TSAT ,
CPMX , XMUX ,
                                                 ,,,,,
                                    ,,,,,
                                                                            ,,,,
       +
                                                                                                       ,
       +
       +
       +
000 000
        LOGICAL
                          DISRUP
        NSTPR = 10
C
```

```
COCO
   CALL FOTIME TO BREAKUP THE TIME STEP FROM DBUNDL INTO SMALLER
INTERVALS BASED ON NSTPR.
6
                               (T(I), DELTT, TR, NSTPR)
          CALL
                    FGTIME
¢
          NSTEP . NSTPR
C
     10 CONTINUE
COD
   FIRST TEST PREVENTS TIME . O FROM BEING A STARTING POINT
                                                                 + 1
          IF
                 ( TR( J ) .EQ. 0.0
                                                )
                                                       J
                                                          .
                                                              3
C
                ( J .LE. NSTEP )
                                                THEN
          IF
C
                 SURTIM :
                               IR
                                    1 1 1
                                              1) - TR ( J )
000000
   MATERIAL PROPERTY ADJUSTMENT NECESSARY FOR FRAGMENTED CHARACTER-
ISTIC SUBROUTINE *FGCHAR* DEPENDING ON THE RELATIONSHIP OF THE
CODLANT TEMPERATURE AND THE SATURATION TEMPERATURE
                                                                THEN
          IF
                 ( COLTMR( 1 ) .GE. TSAT )
C
                 ROCOLD = ROVAP
XMUCD = XMUVAP
C
          ELSE
C
                 ROCOLD - ROCOL
X MUCO - XMUCOL
C
          ENDIF
CCC
    CALL FGCHAR TO DEFINE THE CHARACTERISTICS OF FRAGMENTED BUNDLE
                                            S IZAVR
S TRMR
V INROD
X CHRL
                                                                          ZRMR
AREAR
HITER
KTERM
                                                                                         ZROZMR
HITRG
POROSR
                                                                                                        VINR ,
POROPR ,
                                                           XMASSR
ABSMR
DELTR
KFLUID
                           FGCHAR
                 CALL
                                         (
                                                                                                     .
                                                       ,
                                                                                      ,
                                                                       ,
                                                       ;
                                                                                      ,
                                                                       ,
                                                                                                     ,
         4
                                                                       ,
                                                                                      1
         +
                                                        ,
                                                                       ,
0000
    CALL FRAGTH TO DESCRIBE
                                           THE BEHAVIOR OF
                                                                      THE FRAGMENTED BUNDLE
                                            SIZAVR
ZROZTR
HTLBRD
MAXL
KFLUID
ELVMR
                                                           PORDSR
ZROZAR
HTLBRC
DELTR
EL VA R
DXDAR
                                                                          HITER
ALPHTR
HTUBRD
IDREGR
BEOTMR
FISHR
                                                                                         ALPHAR
HTUBRC
                                                                                                         VINR
EL VNR
ND
                         FRAGTH
                                                                                                                  ۰,
                 CALL
                                         (
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         +
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                                                                                      ,
                                                                                                     ,
                                                                                                         AREAR
THMOTR
FGRSR
                                                                                         NONR
COLTMR
HYDGR
                                                                                      ,
                                                                       ,
                                                                                                     ,
         ٠
         +
                                                        ,
                                                                       ,
                                                                                                                     ,
         4
                                                                       ,
```

,

VOLGSR , IRT , DOWNR , DISRUP) + 0000 COMPUTE LIQUIFIED MATERIAL MOVEMENT IF DEBRIS BED MELTING OCCURS CALL (NONR , IRT , ELVMR , ELVAR , DELTR , FGMELT 000000000 TEST FOR LOWER REGION BOUNDARY BREAKTHROUGH RETURN TO DBUNDL IF BREAKTHRU OCCURS, WITH END OF TIME INTERVAL IF (DISRUP) THEN C NSTEP . J CC ELSE 000 COMPUTE ESTIMATED TIME OF DISRUPTION FGESTT (ELVMR , ELVNR , VELMOT , CURTIM , ESTDT) CALL 00000 IF ESTIMATED TIME OF BREAKTHROUGH IS GREATER THAN CURRENT TIME PLUS ADJUSTED DELTA T, SET CURRENT TIME TO NEXT TIME INTERVAL. IF (ESTDT .GT. TR(J + 1)) THEN 3 CURTIM = TR(J + 1) C ELSE 000000 IF ESTIMATED TIME OF BREAKTHROUGH IS LESS THAN CURRENT TIME PLUS ADJUSTED DELTA T, SET CURRENT TIME TO ESTIMATED TIME AND NEXT TIME INTERVAL TO CURRENT TIME CURTIM = ESTDT TR (J + 1) = CURTIM C ENDIF C ENDIF 0000 WHEN J IS GREATER THAN NSTPR, CONTROL WILL RETURN TO DBUNDL WITH CTIMER CONTAINING THE CURRENT TIME Ga to 10 C ENDIF cc RETURN C END

TABLE A-8. LISTING OF FGTIME

```
CC
          SUBROUTINE FOTIME ( TIMIN , DELTT , TR , NSTP )
SUBCODE NAME: FGTIME
PURPOSE: TO DEFINE THE RUBBLE DEBRIS TIME STEP
CALLING SUBROUTINES: DBFRAG
SUBROUTINES CALLED: NONE
WORK PACKAGE: 15
ENGINEER/PROGRAMMER: S.T.HSIEH/G.H.BEERS
LAST MUDIFICATION DATE: 11/30/81
   INPUT VARIABLES
                                                               DESCRIPTION
                                TIME STEP COMING FROM DISRUPTED BUNDLE TIME STEP
        DELTIN
   OUTPUT VARIABLE
                                                               DESCRIPTION
                                TIME STEP WHICH WILL BE USED IN THE RUBBLE DEBRIS
ANALYSIS - DELTIN PROTECTION OF STEPS INTO WHICH DETIME TIME STEP WILL
BE BROKEN
        DELTCT
        NSTP
         DIMENSION
                                 TR ( NSTP + 1 )
cc
         STEPS . DELTT / FLOAT ( NSTP )
C
          DO 10 I = 1 , NSTP + 1
C
                TR ( I ) = TIMIN + FLOAT ( I - 1 ) * STEPS
C
     10 CONTINUE
C
          RETURN
```

TABLE A-9. LISTING OF FGCHAR

SUBROUTIN	FGCHAR (SIZAVR , XMASSR , ZRMR , ZROZMR , UDZMR , STRMR , ABSMR , AREAR , HITRG , VINR VINROD , DELTR , HITER , PUROSR , PORUPR , XCHRL , KFLUID , KTERM)
PURPOSE	TO DEFINE RUBBLE BED CHARACTERISTICS AND HYDRAULIC
BEHAVIOR	
CALLING S	UBROUTINE DEFRAG
SUBREUTI	E CALLED : NONE
ENGINEER	PROGRAMERISTH
LAST DATE	MODIFIED: 8/10/81
INPUT VA	IABLES:
SIZAVR	AVERAGE PARTICLE SIZE OVER ACCUMULATED MASS AND
XMASSR	TOTAL MASS OF DEBRIS ACCUMULATED FOR ALL COMPONENTS(KG)
ZRMR	TOTAL MASS OF ZIRCALOY ACCUMULATED FOR ALL COMPONENTS
ZROZMR	TOTAL MASS OF ZRD2 ACCUMULATED FOR ALL COMPONENTS(KG)
UD2MR	TOTAL MASS OF UD2 ACCUMULATED FOR ALL COMPONENTS (KG)
STRMR	TOTAL MASS OF CORE STRUCTURE MATERIALS ACCUMULATED (KG)
ABSMR	TOTAL MASS OF CONTROL ROD MATERIAL ACCUMULATED(KG)
AREAR	TOTAL BUNDLE CROSS SECTIONAL AREA(M2)
HITRG	FRAGMENMTED DEBRIS REGION HEIGHT FROM DBREGN(M)
VINR	CODLANT INLET VELOCITY (M/SEC)
VINROD	COOLANT INLET VELOCITY AT PREVIOUS TIMNE STEP, M/SEC
DELTR	TIME STEP(SEC)

DUTPUT HITER	VARIABLES: BED HEIGHT, IF PACKED BED, DELTA H=HITRG-HITER=A VOID AT THE TOP OF PACKED BED(M)
POROSR	BED PORDSITY, FOR MODO POROSR IS AN AVERAGED VALUE OVER THE BED
POROPR	PRESIURE DROP ACCROSS THE BED(PA)
XCHRL	CHARACTERISTIC LENGTH OF THE PARTICLE, DERIVED FROM
KFLUID	FLUIDIZATION FLAG, =0 PACKED BED, =1 FLUIDIZED BED
KTERM	ABNORMAL TERMINATION FLAG, =0 NORMAL RUNS, =1 ABNORMAL TERMINATION
AT THIS THROUGH	TIME, ALL MATERIAL PROPERTIES ARE ASSUMED COMING A COMMON BLOCK, THESE INCLUDE:
ROZR	ZR DENSITY(KG/M3)
ROZRO2	ZRO2 DENSITY(KG/M3)
ROUDZ	UD2 DINSITY(KG/M3)
ROSTR	DENSITY OF STRUCTURAL MATERIAL(KG/M3)
ROABS	DENSITY OF CONTROL ROD MATERIAL (KG/M3)
ROCOL	CODLANT DENSITY (KG/M3)
X MUC OL	VISCOSITY OF CODLANT(KG/SEC/M)

```
ROCOL
HEG
TSAT
XMUX
                                                     ROUO2
DMY2
XKCOL
XLATC
RODEB
                                                                  RONAP
ROMAP
                                                                                RGABS
XMUVAP
CPDEB
CPMX
                                        ROZROZ
DMY1
CPCOL
TMELT
XMUF3
                                                                                           ,
                          ROZR
XMUCOL
SURTC
RUSAT
                                                                             ,,,
                                                                ,
         COMMON
                                                  ,
                                     ;
                                                                                                         ,
                                                  ,
       +
                                                  ,
                                                                                           ,
                                                                                                        ,
                                                                ,
                                     ,
       +
                                                                                           .
                                                                                                         .
                                                                              ,
                                                  ,
                                                                ,
                                     ,
       +
                           XKMX
                                                  .
       +
000
                 3.14159
         PI .
0000
  CALCULATE DEBRIS VOLUNE WITH ZERO POROSITY
       TOTVOL - ZRMR / ROZR + ZROZMR / ROZROZ + UC2MR / ROUDZ + STRMR
+ / ROSTR + ABSMR / ROABS
CCC
   CALCULATE ZERO-POROSITY BED HEIGHT (M)
         HITSOL . TOTVOL / AREAR
000
   CHECK DEBRI'S REGION HEIGHT
         IF ( H TSD: GT. HITRG )
                                                 THEN
C
               WRITE ( 6 , 100 )
C
         ELSE
 CCCC
   DEBRIS BED PACKING IS BASED ON LMFBR EXPERIMENTS
               POROSR = 0.593 - 1.23E-4 * XMASSR / AREAR
 000
   CALCULATE PACKED BED HEIGHT
               HITER - HITSOL / ( 1.0 - POROSR )
 C
                      ( HITER .GE. HITRG ) THEN
HITER - HITRG
POROSR - 1.0 - HITSOL / HITRG
                IF
 C
                ENDIF
 CCC
    CALCULATE MINIMUM FLUIDIZATION VELOCITY (M/SEC)
                ROBED = XMASSR / ( AREAR * HITSOL )
 C
                GMFBC = 688.0 * ( SIZAVR * 39.37 ) ** 1.82 *
( ROCOL * 0.66243 * ( ROBED - ROCOL ) * 0.06243 )
** 0.94 * ( XMUCOL * 1E+03 ) ** (-0.88 )
* 0.4536 / 3600.0 / ( 0.3048 ) ** 2
         ٠
         +
 C
                RENODI . GMFBC . SIZAVR / XMUCOL
```

```
C
                 ( RENOD1 .LT. 7.5731 )
             IF
                                                  THEN
C
                  CORFCT = 1.0
¢
             ELSE IF ( RENOD1 .GE. 7.5731 .AND. RENOD1 .LT. 200.0 ) THEN
C
                  CORFCT = 1.364135 -0.179864 * ALGG ( RENOD1 )
C
             ELSE IF ( RENDD1 .GE. 200.0 .AND. RENDD1 .LT. 1E+03 ) THEN
C
                  CORFCT = 0.214413 + 39.3522 / RENOD1
C
             ELSE IF ( RENOD1 .GE. 1E+03 )
                                                         THEN
C
                  CORFCT . 0.253764
C
             ENDIF
C
                        RENOD1
GMFBC
GMFBC
             RENOD2
                                * CORFCT
* CORFCT
/ ROCOL
                     .
             GMFBC
                      .
COCC
  CHECK PACKED OR FLUIDIZED BED
                            •LE. VELME ) THEN
(VINR - VINROD) * ROCOL / DELTP
150.0 * (1.0 - POROSR) ** 2
(AMAX1(POROSR , 1.0E-6)) ** 3 /
                    ( VINR
XITM1
ALPHA
              IF
                           .
                           .
                            (AMAX1(POROSR , 1.0E-8)) ** 3 / (SIZAVR ** 2 )
1.75 * (1.0 - POROSR)
(AMAX1(POROSR , 1.0E-8)) ** 3 / SIZAVR
                    BETA
                          .
CCC
  CALCULATE XCHRL, CHARACTERISTIC LENGTH OF PACKED PARTICLE
                    XCHRL = BETA / ( AMAX1(ALPHA , 1.CE-8) )
CCC
  CALCULATE PRESSURE DROP, ERGUN'S EQUATION
                   FOROPR = XITM1 + (ALPHA * XMUCOL + BETA * ROCOL

* VINR ) * VINR

PDROPR = PDROPR * HITER
C
                    KTERM . 0
KFLUID . 0
C
              ELSE
                    POROPR = (XMASSR / AREAR - ROCOL * HITSOL) * 9.80665
00000
         ABOVE IS THE CALCULATION OF PRESSURE DROP ACROSS FLUIDIZED BED
  BED PORUSITY ACCORDING TO LEVA'S FLUIDIZATION, 1959, P. 87.
```

ç		
•		RENGD3 * SIZAVR * ROCOL * VINR / XMUCOL DIABND = (AREAR * 4.0 / PI) ** 0.5
С		TE (DENODO IT 0.2.) THEN
С		IF (KENUUS .LI. U.2.) THEN
с		SLOPC = 5.0
~		ELSE IF (RENOD3 .GE. 0.2 .AND. RENOD3 .LT. 1.0) THEN
		SLOPC = (4.35 + 17.5 * SIZAVR / DIABND) * RENOD3 ** (-0.03)
C		ELSE IF (RENOD3 .GE. 1.0 .AND. RENOD3 .LT. 200.0) THEN
c		SLOPC = (4.45 + 18.0 * SIZAVR / DIABND) * RENOD3 ** (-C.1)
C		ELSE IF (RENOD3 .GE. 200.0 .AND. RENOD3 .LT. 500.) THEN
C		SLOPC = 4.45 * RENOD3 ** (-0.1)
C		
с		ELSE IF (RENUDS .GE. DOU.O) THEN
c		SLOPC = 2.39
~		ENDIF
c	•	PORIMT = (RENOD3 / RENOD2 * POROSR ** SLOPC) ** (1.0 / SLOPC)
c		WRITE (6 , 500) RENOD2 , RENOD3 , PORDSR , SLOPC , PORIMT
· .		PORIMT - AMINI (PORIMT : 1.0)
		AMAX1(1.0E-08 , (1.0 - PORINT))
c		POROSR . PORIMT
~		IF (HITER .GE. HITRG) THEN
		HITER - HITRG POR OSR - 1.0 - HITSOL / HITRG
-		ENDIF
c		ALPHA = 150.0 * (1.0 - POROSR) ** 2 / (AMAX1 (POROSR ,
	•	1.0E-8)) ** 3 / (SIZAVR ** 2)
	+	** 3 / SIZAVR
с		XCHRL = BETA / (AMAXI(ALPHA , 1.0E-8))

ç			KELU	ID,	• 0 ¹								
C		ENDIF	DIF										
c	100	FORMAT WRITE(FORMAT	(2X,50 6,700) (2X,6H	HTO	MF MF MF=,E1	MASS 2.4)	IN	RUBBLE	BED,	CHECK	FRAG	MENTED	MASSI
C C	500	+ FOR MAT	E12.5	;	7HREND 6HSLOP	D2:,E C:,E1	12.5	, 7HR	ENOD3 RIMT.	,E12.5	, 71	POROS	R=,
C		RETURN											

TABLE A-10. LISTING OF FRAGTH

SUBROUTINE	FR.	AGTH	(SNETKEN	ZA VR LOZTR LORD LUID VMR LGSR	PNEOWD-	CROZAR TLBR ELTR LVAR	R AL	RETARDAR FLANDAR LANDAR	XCHRL ALPHAR HTUBRC COLTMR HYDGR DISRUP	VINR ELVNR ND AREAR THMOTR FGRSR
		C14 AT						LAUTODE		0.01.5
BED.	U CAL	LUULAI	E 10	EKHAI		RELA	100 50	TAVIURS	UF A RU	DOLL
CALLING SU	BROUT	TINE:	DBFR	OZ						
SUBROUTINE	CAL	LED: T	EMPS	R						
ENGINEER /P	ROGR	AMMERI	5.	HSI	EH					
LAST DATE	MODI	FIED:	8/10	/81						
INPUT VARI	ABLES	\$ 2								
SIZAVR	AVER	AGE PA	RTIC	LE DI	AME	TER	OF A R	UBBLE D	EBRIS(M)	
POROSR	DEBRI	IS BED	POR	OSITI	٢					
HITER	BED H	HEIGHT	(M)							
XCHRL	CHAR	ACTERI	STIC	LENG	STHO	FRU	BBLE B	DOY FRO	M DELT P	, M
VINR	COOL SUPER	ANT IN REICIA Y TUBE	LET BAS ANNE	VELOCI LOCI IS.	TY DI THE NCT ((M/SI F THI TRUE URE)	EC), N E FLUI COOLA	NT VELO	T VINR IS	S THE The
ZROZTR	EFFE	TIVE	ZROZ	READ	TIO	N LA	YER TH	ICKNESS	(M)	
ZROZAR	EFFEC	TIVE	ZR-S	TEAM	REA	CTIC	N AREA	(M2)		
ALPHTR	EFFE	CTIVE	ALPH	A-ZR	REA	CTIO	N LAYE	R THICK	NESS, M	
ALPHAR	EFFEC	CTIVE	ALPH	A-ZR	REA	CTIO	N AREA	(M2)		
ELVNR	EL EV	HE BOT	OF P	UBBLI OF RI	E BO	DY-FI	ROM TH	E BOTTO	M OF ROD	BUNDLE
HTLBRD	HEAT	TRANS	FER	INTO	DEB	RIS	BED AT	LOWER	BOUNDARY	. W/M2
HTLBRC	HEAT	TRANS	FER	INTO	DEB	RIS	COGLAN	T AT LO	WER BOUND	DARY, W/M2
HTUBRD	HEAT	TRANS	FER	INTO	DEB	RIS	BED AT	UPPER	BOUNDARY	W/M2

HTUBRC	HEAT TRANSFER INTO DEBRIS COOLANT AT UPPER BOUNDARY, N/M2
ND	NUMBER OF NODES TO BE USED IN LIQUID OR VAPOR REGION
MAXL	MAXIMUM NUMBER OF NODES IN THE RUBBLE BODY WHICH COMBINED LIQUID, SATURATION AND VAPOR REGION,
DELTR	TIME STEP(S)
AREAR	TOTAL BUNGLE CROSS SECTIONAL AREA,M2
KFLUID	FLUIDIZATION FLAG, =0 PACKED BED, =1 FLUIDIZED BEDF
INPUT/OUT	PUT VARIABLES:
IDREGR	REGION TYPE I.D. =1 VINR GT O ONE LIQUID REGION =2 VINR GT O ONE VAPOR GEGION =3 VINR GT O OND SAT. REGION =4 VINR GT O TWO REGIL & S =5 VINR GT O TWO REGIS & V =6 VINR GT O THREE REG LASEV
	-8 VINE-0 ONE VAPOR REG
NONR	NUMBER OF NEDES USED IN RUBBLE BODY ANALYSIS, =ND IDREGR=1,2,7,8 =3 IDREGR=3 =N D+2 IDREGR=4,5 =2*ND+1 IDREGR=6
ELVAR	ELEVATION OF NODES IN DEBRIS, ELVAR(1)=ELVNR ELVAR(NONR)=ELVNR+HITER
BEDTMR	DEBRIS TEMP_RATURE CORRESPONDING TO NONR NODES
COLTMR	COOLANT TEMPERATURE CORRESPONDING TO NONR NODES
DXDAR	ZR-STEAM HEAT GENERATION RATE (W/M3)
FISHR	FISSION/DECAY HEAT GENERATION RATE (W/M3) MOLTEN CORE REGION ELEVATION AT LOWER BOUNDARY, M
CUT PUT VA	ARIABLES:
THMOTR	MOLTEN MATERIAL THICKNESS(M)
HYDGR	HYDROGEN GENERATION DURING DELTR(MOLES)

.

.

	FGRSR	FISSION GAS RELEASE(MOLES) DURING DELTR
	VOLGSR	VOLATILE FISSION PRODUCTS RELEASE DURING DELTR, MOLE
	IRT	DEBRIS REGION TYPE, •O SOLID REGION, •1 MOLTEN REGION TOTAL OF NONR VALUES
	DOWNR	LENGTH OF MOLTEN POOL PENETRATION, M
		AFTER CURRENT TIME, (S)
	DISRUP	DISRUPTION FLAG
	AT THIS	TIME, ALL MATERIALS PROPERTIES ARE ASSUMED COMING COMMON BLOCK, THESE INCLUDE:
	ROCOL	LIQUID COOLANT DENSITY(KG/M3)
	ROVAP	STEAM DENSITY (KG/M3)
	XMUCOL	LIQUID COOLANT VISCOSITY(KG/SEC/M)
	XMUVAP	VAPOR VISCOSITY (KG/SEC/M)
	HFG	LATENT HEAT OF VAPORIZATION (J/KG) OF COOLANT
	SURTC	SURFACE TENSION OF COOLANT (PA)
11 W	CPCOL	LIQUID SPECIFIC HEAT(J/K/KG)
30.30	XKCOL	LIQUID COOLANT THERMAL CONDUCTIVITY)W/M/K)
¥ ¥	XKVAP	VAPOR(STEAM) THERMAL CONDUCTIVITY(W/M/K)
***	CPDEB	SPECIFIC HEAT OF DEBRIS(J/K/KG)
3000	ROZR	ZR DENSITY(KG/M3)
34.36	ROZRO2	ZRO2 DENSITY(KG/M3)
3030	ROUDZ	UD2 DENSITY (KG/M3)
ic.	ROSTR	DENSITY OF STRUCTURAL MATERIAL (KG/M3)
N. N.	RUABS	DENSITY OF CONTROL ROD MATERIAL (KG/M3)
CCC CCC	RCDEB	DEBRIS BED DENSITY (POROSITY DEPENDENT)

		1)	KM	UD	68	3			V	1 5	C	93	S I	T	Y	0	F	1	E	8	R	IS	()	KG	;/	Si	EC	1	M)																
			ĸĸ	DE	8				T	18	R	MJ	L		cc	IN	0	U	: T	I	V	IT	Y	0	16	í.	E	в	R	IS	(ω.	11	11	K)	6										
11 91 91		1	rs	A T	С				SA		UI	RA	T	IM		i.T	Ţ,	EMK	P	E	R	T	U	2.6		OF		С	01	αι	. A	Ν.	r	٥	F	R	U	BB	LE		DE	8	RI	s		
3. 2		1	20	SA	T				W	1	E	R	0	E	NS	I	T	Y	A	T	5	5 A	TI	JR	A	T	10	N	()	KG	;/	M	3)													
50		1	TM	EL	Т				-	Ē١	. T	11	NG		TI	EM	P	ER	A	T	UF	RE	() F		DE	8	R	1	s	M	A '	T 6	R	IA	L	"	()								
1000			X L	AT	c				L	A 1	E	NT	r	н	E	T		OF		F	U :	SI	0		F	OF	\$	D	Ei	BR	I	S	1	A	TE	R	1,	AL	۱.	31	K	G)				
CC C		+++	I	ME	NS	I	01	4		E ST	LEMC	V	ARM	-040		11))			BCXT	EOKC		MIM		4420	1)		, , ,	-	RE	M	TNXP	1R 4	-0-	41)))		•	L CT	AT.	, × P	14	1020))	;;	
		++++	C G	MM	101	¥				CE AVINA A	OMUOK	ZURSM	TOTAT				RRCTX		ROOLF	DLLT3	2	****	La constanta		DUCAD				,,,,	a a va	OCK	SVVM	TAPP		, ,		RUXIC	DA UDA	BYEX	SAP			RHS		old K	
30 0		ļ	10	GI	c	AL	ľ			1	I	SI	RU	P																																
C			DA	TA			i)	PI		1	3	•	14	1	5	,	1																													
č	CAL	.c	UL	AT	Έ	V	0	LU	M	E 1	R	I	:	н	E	AT	ŕ,	GI	EN	E	R	AT	I		4	R	AT	E	(01	10	L	()	1	M 3	3)										
c					P	:	0	X D	VI	R	+	1	FI	s	н	R																														
č	BAS	E	D			2V			v	II	R	,	,	N	D	c	0	L 1	T M	R	(СН	E	C #	(TH	HE		R	E	I	0	N	I	D											
Č,	020		co	NT	I	NU	E		8			i,			2	1							F,					1				2	ľ		1											
C			XL	LISA	OTP			-1	000	000	000																																			
ç	CAL	.c	UL	AT	E	D	R	10	U	T	H	E	A 1		F	LL	x	,	L	I	P	IN	S	KI		s		10	D	EL																
C		+	C A	LL	. (R	Y	Du	T	1	(V	INCO	R	•	PC	R	0	SRAP		H	IT	E	R	S	I	ZA	V	RD	*		RT		R	, (v	0	L,	R	oc	:0	L,	RC	vc	AP,	

```
C
        IF ( VINR .LT. 0.0 ) THEN
Ce
  COMPARE QUOL TO QDYOUT
             IF ( QVOL * HITER * (1.0-POROSR) .GE. QDYOUT ) THEN
C
             ELSE IDR . 7
C
             ENDIF
C
       ELSE
000
  REGION TYPE 1-6 LEFT TO BE IDENTIFIED
             IF ( COLTMR(1) .GT. TSAT ) THEN
C
             ELSEIF
                        ( COLTMR(1) .EQ. TSAT )
                                                       THEN
C
                       IF
                             ( COLTMR(NONR) .EQ. TSAT ) THEN
C
                        ELSE
CCC
  CALCULATE SATURATION REGION LENGTH
                             XLSAT - ROCOL * VINR * HEG / OVOL
/ AMAXI ( (1.0 - POROSR ) , 1.0E-08 )
IDR - 5
XLVAP - HITER - XLSAT
       ٠
C
                                (XLSAT .GE, HITER) IDR = 3
(COLTMR(NONR) .LT. TSAT) IDR = 3
(QVOL+HITER*(1.0-POROSR) .LT. QDYOUT)
IDR = 3
                             IF
      +
C
                       ENDIF
C
                  ELSE
CCC
  COLTMR(1)
                .LT.
                        TSAT
                        IF (COLTMR(NONR) .LT. "SAT) THEN
¢
                        ELSE
                             XLSAT . ROCOL . VINR
                                         CCOL * VINR * HEG / CVCL
/ AMAX1((1.0 - PORDSR) , 1.0E-8)
      +
C
```

~	IF (XLSAT .GE. HITER) XLSAT = HITER
~	XLLIQ = XLSAT / HFG * CPCDL*(TSAT-COLTMR(1))
	IF (XLLIQ .GE. HITER) XLLIQ = HITER
¢	IF (COLTMR (NON") .EQ. TSAT) THEN
c	XLSAT = HITER - XLLIQ
~	IF (XLSAT .LE. 0.0) IDR = 1
	ELSE IDR = 6 XIVAP = AMAX1 (0.0.(HITER- XLLIG - XLSAT))
C	
	+ .LT. ODYOUT) THEN
c	IDR + HITER - XLLIQ
C	IF (XLSAT .LE. O.C) IDR = 1
8	
	ELSE IF ((XLLIQ+XLSAT) .GE. HITER) THEN
с	XLSAT - HITER -XLLIQ
č	IF (XLSAT .LE. 0.0) IDR = 1
С	ENDLE
С	ENDIE
C	CNOTE
с	
с	ENDIF
с	ENDIF
с	ENDIF
00000	DEBRIS REGION TYPE HAS BEEN FIED, IDR=1-8, IF IDR AND IDREGR ARE NOT CONSISTANT, CALL, BROUTINE REGMOD TO ADJUST TEMPERATURE OF BED AND COULANT, NOULS ELEVATION AND SET IDREGR EQUALS TO IDR
č	IF (IDR .NE. IDREGR) THEN
Ç	CALL REGMOD (IDR, MAXL, ND, IDREGR, NONR, XLLIG, XLSAT, XLVAP,

```
ELVNR, TSAT, HITER, ELVAR, BEDTMR, COLTMR)
         ٠
C
           ENDIF
C
          N2 = ND * 2
C
               50 I = 1 , NONR
          DO
C
                  BEDIMO(I) = BEDIMR(I)
COLTMO(I) = COLTMR(I)
C
     50 CONTINUE
00000000
           BASED ON COLTMR AND BEDTMR, ROMX(N2), CPMX(N2), XMUX(N2) AND
XKMX(N2) ARE KNOWN ASSUME THEY ARE TEMPERATURE DEPENDENT,
FIRST N VALUES ARE FOR BED AND THE REST N VALUES ARE FOR
CODLANT.
           NOW CALCULATE TEMPERATUR OF BED AND COOLANT FOR CURRENT TIME
           IF ( IDREGR .EQ. 1 .OR. IDREGR .EQ. 2 )
                                                                                       THEN
C
                                                              IDYOT :
                          ( IDREGR .EQ. 1 )
( IDREGR .EQ. 2 )
                  IF
                                                                            0
ć
                  VAR1 = 0.0
VAR2 = 0.0
VAR3 = 0.0
VAR4 = 0.0
00000
    CALL MATPRO (BEDTMO, COLTMO, ND, N2, ROMX, CPMX, XKMX, XMUX, KOREGR, IDYOT)
                        100 I = ND + 1 , N2
                  DO
C
                          VAR1 =
VAR2 =
VAR3 =
VAR4 =
                                 • VAR1
• VAR2
• VAR3
• VAR4
                                                 ROMX(I)
CPMX(I)
XKMX(I)
XMUX(I)
                                                                    FLOAT(ND)
FLOAT(ND)
FLOAT(ND)
FLOAT(ND)
                                                                 1
                                              :
                                              *
                                                                 1
Ç
    100
                  CONTINUE
C
                  XREND = VAR1 * VINR * XCHRL / VAR4
XPRDL = VAR2 * VAR4 / VAR3
C
                  XNU = (7.0 - (10.0 - 5.0*PORDSR) * PORDSR) * (1.0 + 0.7

* XREND ** 0.2 * XPRDL ** (1.0/3.G)) + (1.33-(2.4-1.2

* PORDSR) * PORDSR) * XREND ** 0.7 * XPRDL ** (1.0/3.0)
          +
C
                  HVSC = XNU * VAR3 / XCHRL ** 2
CC
```

```
DELTZ - HITER / FLOAT(ND - 1)
C
              IF ( IDYOT .EQ. O .AND. KFLUID .EQ. 1 ) THEN
C
                    IF ( POROSR .LT. 0.25 )
                                                           GO TO 123
C
                    FEBSN = ( 1.0 - (1.0 - POROSR) ** (2.0/3.0) * PI
** (1.0/3.0) * (0.75) ** (2.0/3.0)) ** (-1.0)
000
   XMUF3 IS WATER VISCOSITY AT 300 K FROM MATPRO
                    DIABN = ( 4.0 * AREAR / PI) ** 0.5

XNU = 1.28E-5*(XRENU*FEBSN)**2*XPRDL**(C.67)*(VAR4/

XMUF3)**0.83*(DIABN/XCHRL)**C.5*(RODEB/VAR1)**2

HVSC = XNU * VAR3 / XCHRL ** 2
C
              ENDIF
C
   123
              CONTINUE
C
              IF ( IDYOT .EQ. 1 ) THEN
C
                    HVSC = ( XCHRL * ( 1.0 - PORDSR ) ( 200377 ) ** 1.33 *
C
              ENDIF
C
                                                , N2
, HTLBRD ,
, VINR
, COLTMR ;
                                                                HTLBRC , BEDTMO
HTLBRC , HTUBRD
GVOL , DELTR
                                                                                          COLIMO
HIUBRC
DELIZ
              CALL
                       TEMPSR ( NO
                                                                                      ;
                                     HVSC POROSR ;
                                                                                                    ,
        +
Ç
         ELSE IF
                       ( IDREGR . EQ. 7 .OR. IDREGR .EQ. 8 ) THEN
C
              XNU = 7.0 - ( 10.0 - 5.0 * PORDSR ) * PORDSR
C
               IF ( IDREGR .EQ. 7 )
IF ( IDREGR .EQ. 8 )
                                                 IDYOT : 0
IDYOT : 1
C
              VAR1 = 0.0
0000
   CALL MATPRO ( ......
              DO 200 I = ND + 1 , N2
C
                     VAR1 = VAR1 + XKMX(I) / FLOAT(ND)
C
   200
              CONTINUE
C
              HVSC = XNU * VAR1 / XCHRL ** 2
DELTZ = HITER / FLOAT( ND - 1)
C
```

```
IF ( IDYOT .EQ. 1 ) THEN
C
                          HVSC = ( XCHRL * ( 1.0 - PORDSR ) / .00377 ) ** 1.33 *
XREND ** .65 * VAR3 / XCHRL ** 2
          +
С
                   ENDIF
CC
                                                                 N2
HTLBRD ;
VINR ;
COLTMR ;
                                                                                    IDYOT , BEDTMO ,
HTLBRC , HTUBRD ,
ZVOL , DELTR ,
                                                                                                                 , COLTMO ,
, HTUBRC ,
, DELTZ ,
                              TEMPSR
                   CALL
                                              ( NO
                                                 HVSC
PORDSR
BEDTMR
          +
         +
         +
000000
           IF IDREGR EQUALS TO 3, OVOL IS USED TO HEAT SATURATED WATER
NO BED AND CODLANT TEMPERATURE CHANGES ASSUMED, I.E. NO
CALCULATION OF TEMPERATURE IS NEEDED
           ELSE IF ( IDREGR .EQ. 4 ) THEN
IDYOT • 0
DELTZ • XLLIQ / FLOAT( ND - 1 )
C
                   VAR1
VAR2
VAR3
VAR4
                           - 0.0
00000
   CALL MATPRO ( ... . ... . ...
                   DO
                          300
                                    I = ND + 1 , N2
C
                           VAR1 = VAR1
VAR2 = VAR2
VAR3 = VAR3
VAR4 = VAR4
                                                    ROMX(I)
CPMX(I)
XKMX(I)
XMUX(I)
                                                                        FLUAT(ND)
FLUAT(ND)
FLUAT(ND)
FLUAT(ND)
                                                 +++
                                                                    1111
                                                 +
C
    300
                   CONTINUE
C
                   XRENG = VAR1 * VINR *
XPROL = VAR2 * VAR4 /
                                                            XCHRL / VAR4
C
                   XNU = (7.0 - (10.0 - 5.0*POROSR) *POROSR) * (1.0 + 0.7

* XRENO ** 0.2 *XPRDL ** (1.0/3.0))+(1.33-(2.4-1.2

* POROSR) * POROSR) * XRENO**0.7*XPRDL**(1.0/3.0)
         ++
C
                   HVSC = XNU * VAR3 / XCHRL ** 2
C
                   IF
                         ( KFLUID .EQ. 1 )
                                                                   THEN
C
                           IF ( PORDSR .LT. 0.25 )
                                                                                GO TO 323
C
```

```
FEBSN = (1.0-(1.0 - PORDSR) ** (2.0/3.0) * PI

** (1.0/3.0) * (0.75) ** (2.0/3.0)) ** (-1.0)

CIABN = ( 4.0 * AREAR / PI ) ** (0.5)

XNU = 1.28E-5*(XRENO*FEBSN)*22*XPRDL**0.67*(VAR4 /

XMUF3)**0.83*(DIABN/XCHRL)**0.5*(RDDEB/VAR1)**2

HVSC = XNU * VAR3 / XCHRL ** 2
           +
           +
C
                      ENDIF
C
    323
                      CONTINUE
C
                      DO 400 I = 1 , ND
C
                               TEMPBO(I) - BEDTMO(I)
TCOLTO(I) - COLTMO(I)
C
     400
                      CONTINUE
CC
                                                         NO
HVSC
PORDSR ;
TEMPB ;
                                                                             N2
HTLBRD
VINR
TCOLT
                                                                                                 IDYOT
HTLBRC
OVOL
                                                                                                                     TE MPBO
HTUBRD
DELTR
                                                                                                                                         TCULTO ;
HTUBRC ;
DELTZ ;
                      CALL
                                    TEMPSR
                                                     (
                                                                                                                                    ;
                                                                                           ;
                                                                                                                ;
            4
                                                                                                                  ,
                                                                                                                                     ,
            ٠
                                                                                             3
            4
00
                      DO
                                500 I = 1 , ND
C
                               BEDTMR(I) - TEMPB(I)
COLTMR(I) - TCOLT(I)
C
     500
                       CONTINUE
C
                      BEDTMR (ND+1)
BEDTMR (ND+2)
CULTMR (ND+1)
COLTMR (ND+2)
                                                       AMAX1( BEDIMO( NO + 1 ); BEDIMR( ND ))
AMAX1( BEDIMO( ND + 1 ); BEDIMR( ND ))
COLIMR(ND)
COLIMR(ND)
                                                  .
                                                   .
                                                   :
C
              ELSE IF (IDREGR . EQ.5)THEN
C
                       IDYOT = 1
DELTZ = XLVAP / FLOAT( ND - 1 )
C
                       VAR1 = 0.0
VAR2 = 0.0
VAR3 = 0.0
VAR4 = 0.0
00000
     CALL MATPRO (
                                    ... ,
                                                ... ,
                                                             ...
                       DO
                             600
                                         I = ND + 1 , N2
 C
```

```
VAR1 = VAR1 + ROMX(I) / FLOAT(ND)
VAR2 = VAR2 + CPMX(I) / FLOAT(ND)
VAR3 = VAR3 + XKMX(I) / FLOAT(ND)
VAR4 = VAR4 + XMUX(I) / FLOAT(ND)
C
   600
                  CONTINUE
C
                  XREND = VAR1 * VINR * XCHRL / VAR4
XPRDL = VAR2 * VAR4 / VAR3
C
                  XNU = (7.0 - (10.0 - 5.0*POROSR) * POROSR) * (1.0+0.7
* XRENO ** 0.2 * XPROL ** (1.0/3.0))+(1.33-(2.4-1.2
* POROSR)* POROSR)* XRENO ** 0.7 * XPROL**(1.0/3.0)
         +
         +
C
                   HVSC = XNU * VAR3 / XCHRL ** 2
C
                   00
                        700 I = 1 , ND
C
                          TEMPBO(I) = BEDIMO(I+2)
TCOLTO(I) = COLTMO(I+2)
C
    700
                   CONTINUE
C
                        ( IDYOT .EQ. 1 )
                   IF
                                                             THEN
C
                          HVSC = (XCHRL * ( 1.0 - PORDSR ) / .00377 ) ** 1.33 *
XREND ** .65 * VAR3 / XCHRL ** 2
C
                   ENDIF
CC
                                                NO , N2 , IDYOT , TEMPBO , TCOLTO
HVSC , HTLBRO , HTLBRC , HTUBRO , HTUBRC
POROSR , VINR , OVOL , DELTR , DELTZ
TEMPB , TCOLT )
                              TEMPSR
                   CALL
                                              (
         ++
                                                                                                                                  .
          +
ç
                   DO 800 I = 1 , ND
C
                          BEDTMR(I+2) = TEMPB(I)
COLTMR(I+2) = TCOLT(I)
C
    800
                   CONTINUE
C
                   COLTMR(1) = COLTMR(3)
COLTMR(2) = COLTMR(3)
C
                   BEDTMR(1) = AMAX1( BEDTMO( 1 ) , BEDTMR( 3 ))
BEDTMR(2) = AMAX1( BEDTMO( 2 ) , BEDTMR( 3 ))
C
            ELSE IF ( IDREGR .EQ. 6 )
                                                                  THEN
C
                   IGYDT . O
```

```
DELTZ = XLLIQ / FLOAT( ND - 1 )
C<sub>1200</sub>
                  VAR1 = 0.0
VAR2 = 0.0
VAR3 = 0.0
VAR4 = 0.0
                           : 0.0
000000
    CALL MATPRO ( ... , ... , ...
                         900
                                 I = ND + 1 , N2
                  00
C
                         VAR1
VAR2
VAR3
                          VAR1 - VAR1 + ROMX(I) / FLOAT(ND)
VAR2 - VAR2 + CPMX(I) / FLOAT(ND)
VAR3 - VAR3 + XKMX(I) / FLOAT(ND)
VAR4 - VAR4 + XMUX(I) / FLOAT(ND)
C
    900
                  CONTINUE
C
                  XREND = VAR1 * VINR * XCHRL / VAR4

XPRDL = VAR2 * VAR4 / VAR3

XNU = (7.0 - (10.0 - 5.0*POROSR) * POROSR)*(1.0+0.7

* XRENO ** 0.2 * XPRDL**(1.0/3.0))+(1.33-(2.4-1.2

* POROSR) * POROSR) * XRENO**0.7*XPROL**(1.0/3.0)
          4
C
                  HVSC = XNU * VAR3 / XCHRL ** 2
C
                  IF
                          ( IDYOT .EQ. O .AND. KFLUID .EQ. 1 )
                                                                                               THEN
C
                          IF ( POROSR .LT. 0.25 )
                                                                           GO TO 923
C
                                       ( 1.0 - (1.0 - PORDSR) ** (2.0/3.0) * PI
** (1.0/3.0) * (0.75) ** (2.0/3.0)) ** (-1.0)
                          FEBSN .
                                      **
          ٠
000
    XMUF3 IS THE WATER VISCOSITY AT 300 K FROM MATPRO
                          DIABN = ( 4.0 * AREAR / PI) ** (0.5)
C
                         XNU = 1.28E-5 * (XRENU * FEBSN) ** 2
* XPRDL ** 0.67 * (VAR4 / XMUF3) ** 0.83 *
(DIABN / XCHRL) ** 0.5 * (RODEB / VAR1 ) ** 2
          4
C
                         HVSC = XNU * VAR3 / XCHRL ** 2
C
                  ENDIF
C
    923
                  CONTINUE
CC
                  DO 1000 I = 1 , ND
C
```

```
TEMPBO(I) = BEDTMO(I)
TCCLTO(I) = COLTMO(I)
c1000
                  CONTINUE
                                           ( ND , N2
HVSC , HTLBRD ,
POROSR , VINR ,
TEMPB , TCOLT )
                                                                               IDYOT , TEMPBO
HTLBRC , HTUBRD
GVOL , DELTR
                                                                                                               HTUBRC ;
DELTZ ;
                  CALL
                             TEMPSR
                                                                                                          ;;
         +
         ++
8
                  DO
                         1100 I = 1 , ND
С
                         BEDTMR(I) = TEMPB(I)
COLTMR(I) = TCOLT(I)
c1100
C
                  CONTINUE
                  SEDIMR(ND+1) = AMAX1(BEDTMO( ND+1 ), BEDTMR( ND ))
COLTMR(ND+1) = COLTMR(ND)
C
                  IDYOT = 1
DELTZ = XLVAP / FLOAT( ND - 1 )
0000
           CODLANT PROPERTIES ARE VAPOR PORPERTIES NOW
                  VAR1 = 0.0
VAR3 = 0.0
00000
    CALL MATPRO ( .........
                  DO 1310 I = ND + 1 , N2
с
                         VAR3 = VAR3 + ROMX (1) / FLOAT { NO }
C<sub>1310</sub>
                  CONTINUE
CC
                  IF ( IDYOT .EQ. 0 ) GO TO 1600
Ç
                  DO
                        1400 I . 1 . ND
C
                         \begin{array}{c} \text{TEMPBO(I)} = \text{BEDIMO} \left\{ \begin{array}{c} \text{I} + \text{ND} + 1 \end{array} \right\} \\ \text{TCOLTO(I)} = \text{COLTMO} \left\{ \begin{array}{c} \text{I} + \text{ND} + 1 \end{array} \right\} \end{array}
C
  1400
                  CONTINUE
Ċ
                  IF
                       ( IDYOT .EQ. 1 ) THEN
C
```

```
HVSC = ( XCHRL * ( 1.0 - PORDSR ) / .00377 ) ** 1.33 *
XREND ** .65 * VAR3 / XCHRL ** 2
       +
C
              ENDIF
CC
                                                 N2
HTLBRD ;
VINR
TCOLT ;
                                                             HTLBRC , HTUBRD , HTUBRC ,
OVOL , DELTR , DELTZ ,
              CALL
                      TEMPSR
                                  (
                                    ND
                                              ,
                                    HVSC
POROSR ;
TEMPB ;
       +++
CC
              DO 1500 I . 1 , ND
C
                    BEDIMR(I+ND+1) = TEMPB(I)
COLTMR(I+ND+1) = TCOLT(I)
c<sup>1500</sup>
              CONTINUE
  1600
              CONTINUE
C
         ENDIF
000
         CHECK DEBRIS BED TEMPERATURE AND DEFINE MELTING REGION
         ING = 0
ISG = 0
DDWNR = 0.0
C
         DD
             2000 I = 1 , NONR - 1
C
              IF ( (BEDTMR(I)+BEDTMR(I+1))/2.0 .GT. TMELT ) THEN
COCO
         TMELT IS DEBRIS BED MELTING TEMPERATURE FROM MAPRO
                    IMG = IMG + 1
JUP = I + 1
IRT(I) = 1
C
              ELSE
                    ISG . ISG + 1
IRT(I) . 0
C
              ENDIF
C
  2000 CONTINUE
C
         IRT( NONR ) = IRT( NONR - 1 )
C
         DO 2010 I = 1 , NONR - 1
Ċ
              J = NONR - I
DTMP1 = ( BEDTMR(J+1) + BEDTMR(J)) / 2.0 - TMELT
```

```
C
                                                                                   ( DTMP1 .LT. 0.0 ) THEN
                                                            IF
C
                                                           ELSE
DOWNR = DOWNR + DTMP1 * ( ELVAR(J+1)
- ELVAR (J) ) * CPDEB / XLATC
                              +
C
                                                                                    BEDTMR(J+1) = TMELT
BEDTMR(J) = TMELT
C
                                                            ENDIF
C
                                                            IF ( J .EQ. 1 ) GO TO 2010
CC
                                                            IF ( IRT(J) .GT. IRT(J-1) ) THEN
000
                                    MOLTEN MATERIALS MELTING THE LOWER NODE
                                                                                    IF (DOWNR .GT. (0.5*(ELVAR(J)-ELVAR(J-1))) THEN
C
                                                                                                             BEDTMR (J) . IMELI
                                                                                                             \frac{1}{1} \frac{1}{1} = 1
\frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} = \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1} \frac{1}{1
C
                                                                                    ENDIF
C
                                                           ENDIF
C
       2010 CONTINUE
000
                                    THMOTR = 0.0
C
                                    IF ( IRT (1) .EQ. 1 ) THEN
THMOTR - THMOTR + 0.5 * ( ELVAR (2) - ELVAR (1) )
000
            SET DISRUPTION FLAG WHEN DEBRIS REGION TYPE . 1, INDICATING MELTING
                                                             DISRUP . . TRUE.
C
                                    ENDIF
C
                                                            ( IRT ( NONR ) .EQ. 1 ) THEN
THMOTR = THMOTR + 0.5 * ( ELVAR (NONR) - ELVAR ( NONR - 1 ))
                                      IF
C
                                    ENDIF
 C
                                     DD 3020 I = 2 , NONR - 1
 C
```

```
( IRT (I) .EQ. 1 ) THEN
THMOTR - THMOTR + 0.5 * ( ELVAR (I + 1) - ELVAR (I - 1))
             IF
C
            ENDIF
C
 3020 CONTINUE
NOW ADJUSTED BED TEMPERATURE AND MELTEN REGION HAS BEEN DEFINED
      CALL CHEMHT(ZRO2TR, ZRO2AR, ALPHTR, ALPHAR, IDREGR, NONR, BEDTMR,
COLTMR, ELVAR, DELTR, OXDAR, HYDGR)
       CALL NUCLHT(IDREGR, NONR, BEDTMR, ELVAR, DELTR, TOTIME, ... ETC)
       OVOLN = DXDAR + FISHR
IITMP = IITMP + 1
C
           ( IITMP .GT. 50 ) THEN
       IF
C
 2050 FORMAT (2X, 57HITERATION MORE THAN 50 TIMES NO CONVERGENCE IN TEM
C
            GO TO 2030
C
       ENDIF
C
            ( ABS((QVCLN-QVOL)/QVOLN) .GT. 0.05 ) THEN
QVOL = QVCLN
GO TO 2020
       IF
C
       ENDIF
C
 2030 RETURN
```

TABLE A-11. LISTING OF FGMELT

CC SUBROUTINE FOMELT (NONR , IRT VELMOT) , ELVMR , ELVAR , DELTR , SUBCCDE NAME: FGMELT PURCHOSE: TO MEASURE THE LIQUID MATERIAL MOVEMENT WHEN DEBRIS BED MELTING OCCURS. CALLING SUBROUTINES: DBFRAG SUBROUTINES CALLED: NONE WORK PACKAGE: 15 ENGINEER/PROGRAMMER: S.T.HSIEH/G.H.BEERS LAST MODIFICATION DATE: 11/30/81 S.T.HSIEH/G.H.BEERS 11/30/81 LAST MODIFICATION DATE: DESCRIPTION NUMBER OF NODES USED IN RUBBLE BODY ANALYSIS DEBRIS REGION TYPE: = O, SCLID REGION = 1, MOLTEN REGION ELEVATION OF NODES IN CEBRIS TIME STEPS (S) INPUT VARIABLES ELVAR OUTPUT VARIABLES VELOCITY OF MOLTON POOL FLOWING DOWNWARD (M/S) DIMENSIUN ELVAR(NONR) , IRT(NONR) COCC SAVE INCOMING ELEVATION OF MOLTON MATERIAL ELVMO = ELVMR C 100 IF (IRT(II DO GO TO 110 100 CONTINUE C 110 IF (I .LE. NONR) ELVMR = ELVAR(I) C VELMOT = AMAX1(0.0 , (ELVMO - ELVMR)) / DELTR C RETURN

TABLE A-12. LISTING OF FGESTT

C SUBROUTINE	FGESTT (ELVMR , ELVNR , VELMOT , CURTIM , ESTDT																								
C SUBCODE NAME: C PURPOSE: TO E C CALLING SUBROU C SUBROUTINES CA C WORK PACKAGE: C ENGINEER/PROGR C LAST MODIFICAT	FGESTT STIMATE THE TIME OF DISRUPTION TINES: DBFRAG LLED: NONE 15 AMMER: S.T.HSIEH/G.H.BEERS ION DATE: 11/30/81																								
C INPUT VARIABLE C ELVMR C ELVMR C ELVNR C VELMOT C VELMOT C CURTIM	S MOLTEN CORE REGION ELEVATION AT LOWER BOUNDARY ELEVATION OF RUBBLE BODY FROM THE BOTTOM OF ROD BUNDLE TO BOTTOM OF RUBBLE BODY REGION (M) VELOCITY OF MOLTEN POOL FLOWING DOWNWARD (M/S) CURRENT TIME (S)																								
C OUTPUT VARIABL	ES ESTIMATED TIME OF DISRUPTION (S)																								
C TESTBB A ESTDT CU C RETURN END	BS(ELVMR - ELVNR) / AMAX1(1.0E-08 , VELMOT) RTIM + TESTBB																								
	+RC	BRO		IN	EAP	DR	YO		VI X	NC	P P C	JRC , H	SC	,HI	TEO	,E0	FF		; PC	ROP	с,	AVOL	,		
-------	-----	-----	---------------	-----	------	-----	--------	-------------------	------------	-----	------------	------------	-------------	------------------	-------------------	-----	----------	------	------	------	-----	--------------	------------	-------------	------
	PR	CPI	DS E	i.	TC	1-	AL	CUI	DEL	8	DEN	VRI	s	BED	0	RYD	UT	HE	AT	FLU	X	BASE	D	N	
ç	CA	LLI	ING	s	UB	RO	UT	IN	s:	F	RO	ТН	,F	RAG	TH										
c	su	BRI	JUT	IN	3	CA	LL	ED		SM	NM)	(0	F	IMS	L										
ç	EN	GI	NEE	R/	PR		RA	MM	RI	S	ТН														
č	LA	ST	DA	TE		100	IF	IE	:	91	10/	181	çi,												
c	IN	PU	T V	AR	IA	BL	ES	:																	
00000	VI	NC			0000		LARYNC	NT FIC		LE	VEL ASI	VEL OC	I I T	ITY Y O HE	(M/ F T TRL	SE	c) c0		DT	VEL			THI N I	AN NCT (URE)
C	PO	RO	sc		C	EB	RI	SI	BED	Ρ	ORC	ISI	TY												
C	HI	TE	5		B	BED	H	EI	GHT	(1)														
c	EF	FD	IA		E	FF	EC	TI	Æ	PA	RTI	ICL	E	DIA	MET	ER	0	FA	PC	ROUS	s	BODY	, M		
C	PD	RDI	PC		F	RE	SS	URI	E D	RO	P	CR	os	S T	HE	BE	D,	PA							
C	RD	co	L		L	.10	UI	D	:00	LA	NT	DE	NS	ITY	(KG	5/M	3)								
CC	RO	VA	Ρ		١	AP	OR	DI	ENS	IT	Y ()	G	MB)											
ç	XM	UCI	JL		L	.10	UI	0	c00	LA	NT	VI	sc	OSI	TY	KG	15	EC/	-						
L'CC	XM	UV	AP		١	AP	OR	۷	ISC	os	IT		GI	SEC	/M))									
č	HF	G			٤	AT	EN	T	HEA	T	OF	VA	PO	RIZ	ATI		11	KG)						
č	SU	RT	С		5	SUR	FA	CE	TE	NS	IO	NC	F	coo	LAN	11	PA)							
C	QV	OL			١	VOL	UM.	ET	RIC	н	EAT	r G	EN	ERA	TIC	N	RA	TE (W/!	13)					
ç	OU	TP	UT	VA	RI	IAB	LE	s:																	
ç	QD	YO	UT		C	DRY	rou	T	HEA	T	FLU	JX,	W	/ 12											
c	DI	ME	NSI		•			SE	FF (10	0)		,	QX3	(10	00)									
č	00		c - (wo			TC	· •		0-															
ç	VA	DV	3 - 4 T N/				00	с. т .			-1	0	101		-										
č	¥.	~ 1	THE			rr.	00				-1	•••	14	96	• •	AU	KI		-	CAL	FL				
с	DO		100)	1	•	1	,	100																
10	5		SEF	FEE	I			.0 0L	· *	F	LOL NC	AT (I) HF	G											
6			IF	(90	GUE	s	.L	τ.	VA	PE	G J		XI	TE	11	•	(-	-1.0	* (0	X	ITEM	1		
č	:	:	AMA			1.0	1.	75,8,	POP (1.	65	1:	o,- SEF	**	OR0	sc	HFG	/*	EFF	SE		°,*	/ RC *3+X	NA IT	Êm1)	

```
C
                XITEM2 = 180. * ( 1.0 - "OROSC ) ** 2 / EFFDIA ** 2
/ ( AMAX1( 1.0E-8 POROSC ))
** 3 / HFG * ( XMUVAP / ROVAP
/ ( AMAX1 ( 1.0E-8 , ( 1.0 - SEFF(I))) ) ** 3
* SEFF(I) ** 3 + XMUCOL / ROCOL )
        +
        +
        +
C
                XITEM3 = 3.5 * (1.0 - POROSC) * ROCOL * VINC / EFFDIA
/( AMAX1( 1.0E-6 , POROSC ) ) ** 3 / HFG * XITEM1
C
                XITEMB = XITEM2 - XITEM3
C
                XITEM4 = ( -1.0) * (ROCOL-ROVAP) * 9.80665 * SEFF(I) ** 3
- 180. * ( 1.0 - POROSC ) ** 2 * XMUCOL * ROCOL * VINC
/ EFFDIA ** 2 / (AMAX1(1.0E-8 , PCROSC)) ** 3 / ROCOL
        +
C
                 XITEMC = XITEM4 + 1.75 * (1.0-PORDSC)*(ROCOL*VINC) **
    / EFFDIA / ( AMAX1(1.0E-8 , PORDSC) ) ** 3 * XITEM1
000
          NOW SOLVE THE EQUATION A * Q ** 2 + B * Q + C = O FOR Q
                 XITEM5 = XITEMB ** 2 - 4.0 * XITEMA * XITEMC
C
                 IF
                     ( XITEM5 .LT. 0.0 )
                                                          THEN
0000
                        WRITE ( 6 , 200 ) SEFF(I)
FORMAT (2X, 31HNO REAL SOLUTION FOR Q AT SEFF=, F1G. 3)
    200
                        QX3(I) = -1.0
0000
          QX3=-1.0 MEANS THERE IS NO REAL SOLUTION FOR Q
SET QX3(I)=MASS FLUX+HFG
                       GD TO 100 * ROCOL * HFG
C
                 ELSE
                        OX1 = ( -XITEMB + XITEM5
OX2 = ( -XITEMB - XITEM5
                                                               ** 0.5 ) / 2.0 / XITEMA
** 0.5 ) / 2.0 / XITEMA
                        QX3(I) = AMAX1( 0.0 , QX1 , QX2 )
C
                 ENDIF
C
                 IF ( ITR .GT. 30 ) THEN
00000
   WRITE(6,600)
600 FORMAT(2X,69HQX3 VALUE DSCILLATES AROUND VAPEG,SET QX3 VALUE AT TH
+E VALUE OF VAPEG)
                        QX3(I) = VAPEG

QGUES = QX3(I)
C
                        GO TO 100
C
                 ELSE
                        IF ( XITEM1 .LT. 0.0 )
                                                                   THEN
000
          CHECK IF QX3 STILL .LT. VAPEG, IF NOT GO BACK TO ADJUST XITEM1
                                     QX3(I) .GE. VAPEG )
QGUES = QX3(I)
ITR = ITR + 1
GD TD 105
                                                                             THEN
                               IF
                                   1
C
                              ENDIF
C
                        ELSE
```

000 CHECK IF QX3 STILL .GE. VAPEG, IF NGT GD BACK TO ADJUST XITEM1 (QX3(I) .LT. VAPEG) QGUES = QX3(I) ITR = ITR + 1 GQ TQ 105 IF THEN C ENDIF С ENDIF C ENDIF C QGLES = QX3(I) C 100 CONTINUE 000000000 FOR MODEL TESTING, PRINT ALL SEFF AND 9X3, AND FIND MAXIMUM 9X3 WHICH CORRESPONDING TO THE DRYDUT HEAT FLUX AT GIVEN SEFF WRITE(6,30C)(SEFF(I),I=1,10C) WRITE(6,4CO)(QX3(I),I=1,10C) 300 FORMAT(5X,5HSEFF=,10(/10X,10F12.4)) 400 FORMAT(5X,5HQX3=,10(/10X,10E12.5)) 00000 USE IMSL UTILITY SUBROUTINE USMNMX TO FIND THE LARGEST VALUE OF QX3(-QDYOUT). LATER ON A SIMPLE CODING MAY BE USED TO REPLACE IMSL SUBROUTING USMNMX TO AVOID THE UNAUTHORIZED TRANSFER OF IMSL. NTST = 100 INC = 1 C CALL USMNMX (QX3 , NTST , INC , XMIN , QDYOUT) C 500 FORMAT (2X , 17HORYOUT HEAT FLUX=, E13.6) C RETURN

C

C

C

C

C

C

C

```
SUBROUTINE REGMOD(IDR, MAXL, ND, IDREGN, NEND, XLLIQ, XLSAT, XLVAP,
+ELVNC, TSAT, HITEC, ELVAY, BEDTMP, COLTMP)
    PURPOSE: TO MODIFY NODE ELEVATION, TEMPERATURE AND REGION ID NUMBE
    CALLING SUBROUTINE: FROZTH, FRAGTH
    SUBROUTINE CALLED: NONE
    ENGINEER/PROGRAMMER : STH
    LAST DATE MODIFIED: 8/10/81
    INPUT VARIABLES:
                REGION ID NUMBER CALCULATED IN FROZTH OR FRAGTH
    IDR
    MAXL
                MAXIMUM NUMBER OF NODES IN THE ANALYSIS
    ND
                NUMBER OF NODES IN LIQUID OR VAPOR REGION ANALYSIS
                REGION ID NUMBER OF LAST TIME STEP
    IDREGN
                NUMBER OF TOTAL NODES IN THE ANALYSIS
    NOND
    XLLIQ
                LIQUID REGION LENGTH, M
    XLSAT
                SATURATION REGION LENGTH, M
    XL' AP
                VAPOR REGION LENGTH, M
    ELVNC
                ELEVATION OF DEBRIS BED-FROM BOTTOM OF ROD
BUNDLE TO THE BOTTOM OF DEBRIS BED, M
    TSAT
                COOLANT SATURATION TEMPERATURE, K
    HITEC
                DEBRIS BED HEIGHT, M
    INPUT/OUTPUT VARIABLES:
    ELVAY
                ELEVATION OF NOND NODES, M
                BED TEMPERATURE CORRESPONDING TO NOND NODES, K
    BEDTMP
    COLTMP
                COOLANT TEMPERATURE CORRESPONDING TO NOND NODES, K
    DIMENSION ELVAY(41) . BEDTMP(41) . COLTMP(41) . BEDTO(41) .
COLTO(41) . ELVO(41) . COEF(40,3)
    DO
        100
               I = 1 , NOND
         BEDIC( I ) = BEDTMP( I )
COLTO( I ) = COLTMP( I )
         ELVO( I ) = ELVAY( I
                                  )
100 CONTINUE
       ( IDR .LE. 2 .OR. IDR .GE. 7 )
NDR = ND
    IF
                                              THEN
         DO 200 I = 1 , NDR
              ELVAY(I) . ELVNC + HITEC / FLOAT(NOR-1) * (I-1)
200
         CONTINUE
```

```
C
            IF ( ABS( ELVAY( NDR ) - ELVD( NOND )) .LE. 1.0E-10 ) THEN ELVAY( NDR ) - ELVD( NOND )
C
            ENDIF
C
            CALL ICSCCU ( ELVO , COLTO , NOND , COEF , 40 , IER )
000
       WRITE ( 6 , 1000 ) IER
            CALL ICSEVU ( ELVO, COLTO, NOND, COEF, 40, ELVAY, COLTMP, NOR; IER)
C
       WRITE ( 6 , 1000 ) IER
5
            CALL ICSCCU ( ELVO , BEDTO , NOND , COEF , 40 , IER )
000
       WRITE ( 6 , 1000 ) IER
                           ( ELVO , BEDTO , NOND , COEF , 40 , ELVAY ,
BEDTMP , NOR , IER )
            CALL ICSEVU
00000
       WRITE ( 6 , 10000 ) IER
            NOND . NDR
IDREGN . IDR
C
       ELSE IF ( IDR .EQ. 3 )
                                        THEN
Ċ
            DO 300 I . 1 , NDR
C
                 ELVAY(I) = ELVNC + HITEC / 2.0 * (I-1)
COLTMP(I) = TSAT
C
   300
            CONTINUE
C
            IF ( ABS( ELVAY( NDR ) - ELVO( NOND )) .LE. 1.0E-10 ) THEN
C
                 ELVAY( NDR ) . ELVO( NOND )
C
            ENDIF
cc
            CALL ICSCCU ( ELVO , BEDTO , NOND , CDEF , 40 , IER )
000
        WRITE ( 6 , 1000 ) IER
            CALL ICSEVU ( ELVO , BEDTO , NOND , CDEF , 40 , ELVAY ,
BEDTMP , NDR , IER )
0000
        WRITE ( 6 , 1000 ) IER
            NUND . NDR
IDREGN . IDR
C
        ELSE IF ( IDR .EQ. 4 ) THEN
C
            DC 400 I = 1 , ND
C
                 ELVAY(I) = ELVNC + XLLIQ / FLOAT(ND-1) * (I-1)
COLTMP(I) = COLTO(1)+(TSAT-COLTO(1))/FLOAT(ND-1)*(I-1)
C
  400
           CONTINUE
```

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```
C
            ELVAY(ND+1) - ELVNC + (HITEC + XLLIG) / 2.0
ELVAY(ND+2) - ELVNC + HITEC
C
            COLIMP(ND+1) : ISAT
C
            IF ( ABS( ELVAY( NOR ) - ELVO( NOND )) .LE. 1.0E-10 ) THEN
C
                  ELVAY( NDR ) = ELVO( NOND )
C
            ENDIF
C
            CALL ICSCCU ( ELVO , BEDTO , NOND , COEF , 40 , IER )
000
       WRITE ( 6 , 1000 ) IER
                             ( ELVO , BEDTO , NOND , COEF , 40 , ELVAY ,
BEDTMP , NDR , IER )
            CALL ICSEVU
0000
       WRITE ( 6 , 1000 ) IER
            NOND = NDR
IDREGN = IDR
C
       ELSE IF ( IDR .EQ. 5 )
                                      THEN
CC
            COLIMP(1) : ISAT
C
            ELVAY(1) . ELVNC + XLSAT / 2.0
C
            DO 500 I = 3 , NDR
C
                 COLTMP(I) = TSAT+(COLTO(NOND)-TSAT)/FLCAT(ND-1)*(I-3)
ELVAY(I) = ELVNC+XLSAT+(HITEC-XLSAT)/FLCAT(ND-1)*(I-3)
C
   500
            CONTINUE
C
            IF ( ABS( ELVAY( NDR ) - ELVO( NOND )) .LE. 1.0E-10 ) THEN
С
                 ELVAY( NDR ) = ELVO( NOND )
 C
             ENDIF
 C
            CALL ICSCCU ( ELVO , BEDTO , NOND , COEF , 40 , IER )
COC
        WRITE ( 6 , 1000 ) IER
             CALL ICSEVU ( ELVO , BEDTO , NOND , CDEF , 40 , ELVAY ,
BEDTMP , NOR , IER )
 CCC
        WRITE ( 6 , 1000 ) IER
             NOND . NOR
IDREGN . IDR
 C
        ELSE IF ( IDR .EQ. 6 ) THEN
 CC
```

.

```
NDR = 2 * ND + 1
¢
            DO 800 I - 1 , ND
C
                 C
  800
            CONTINUE
C
            COLTMP(ND+1) = TSAT
ELVAY(ND+1) = ELVNC + XLLIQ + XLSAT / 2.0
С
            DO 900 I = 1 , ND
C
                  COLTMP(ND+1+I) = TSAT + (COLTO(NOND) - TSAT)
                 ELVAY(ND+1+I) = ELVNC+XLLIQ+XLSAT+(HITEC-XLLIQ-XLSAT)
/ FLOAT (ND - 1) * (I - 1)
      +
      +
Ç
   900
             CONTINUE
C
             IF ( ABS( ELVAY( NDR ) - ELVO( NOND )) .LE. 1.0E-10 ) THEN
С
                  ELVAY( NDR ) = ELVO( NOND )
C
             ENDIF
C
             CALL ICSCCU ( ELVO , BEDTO , NEND , COEF , 40 , IER )
0000
                10
                        318 }
                                 (ELVO(I), I = 1, NOND)
(BEDTO(I), I = 1, NOND)
        WRITE
                     ;
                    2X , 5HELVO=, 5(/2X , 10F11.6))
2X , 6HBEDTO=, 5(/2X , 10F11.3))
  910 FORMAT
920 FORMAT
000
        WRITE ( 6 , 1000 ) IER
 1000 FORMAT ( 2X , 4HIER= , 12 )
Ċ
                    ICSEVU ( ELVO , BEDTO , NOND , COEF , 40 , ELVAY ,
BEDTMP , NDR , IER )
             CALL
      +
0000
                                 ( ELVAY(I) ; I = 1 ; NDR )
( BEDTMP (I) ; I = 1 ; NDR )
        WRITE
                        930 )
                 66
                     ;
   930 FORMAT ( 2X ; 6HELVAY - , 5(/2X , 10F11.6))
940 FORMAT ( 2X ; 7H3EDTMP= , 5(/2X , 10F11.3))
00000
        WRITE ( 6 , 1000 ) IER
       NOND = NDR
IDREGN = IDR
ENDIF
RETURN
END
```

TABLE A-15. LISTING OF TEMPSR

SUBROUTINE	E TEMPSR (N ; N2 HVSC ; HTLBCD ; HTLBCC ; HTLBCD ; TCOLCO ; POROSC ; YINC ; QVOL ; DELTT ; DELTZ ;	
PURPOSE: 1	TO CALCULATE COOLANT AND BED TEMPERATURE ALONG Z	
CALLING SU	JBROUTINE:FROZTH	
SUBROUTINE	E CALLED: MINERVA	
ENGINEERIF	PROGRAMMERISTH	
LAST DATE	MCDIFIED: 8/ 10/ 81	
INPUT VARI	IABLES:	
N	NUMBER OF AXIAL NODES	
N2	2*N FOR SOLVING COOLANT AND BED TEMPERATURE SIMULTANEOUSLY	
IDYOT	INDICATER OF COOLANT STATE, =0 LIQUID, =1 VAPOR	
TEMPCO	BED TEMPERATURES AT N NODES AT PREVIOUS TIME STEP(K)	
TCOLCO	COOLANT TEMPERATURE AT N NODES AT PREVIOUS TIME STEP(K)	
HVSC	HEAT TRANSFER COEFFICIENT BETWEEN BED AND COOLANT, VOLUMETRIC, W/K/M3	
HTLBCD	HEAT TRANSFER INTO DEBRIS BED AT LOWER BOUNDARY, W/M2	
HTLBCC	HEAT TRANSFER INTO DEBRIS COOLANT AT LOWER BOUNDARY, W/M2	
HTUBCD	HEAT TRANSFER INTO DEBRIS BED AT UPPER BOUNDARY, W/M2	
HTUBCC	HEAT TRANSFER INTO DEBRIS COOLANT AT UPPER BOUNDARY, W/M2	
PERESC	DEBRIS BED PORDSITY	
VINC	COOLANT INLET VELOCITY, M/SEC, NOTE THAT VINC IS THE SUPERFICIAL VELOCITY OF THE FLUID MESURED ON AN EMPTY TUBE BASIS. IN TEMPSR CALCULATION, COOLANT VELOCITY IS THE TRUE VELOCITY IN COOLANT CHANNELS, THEREFORE, VINCT(URE) = VINC/POROSC. THIS ADJUSTMENT IS CALCULATED IN THE FIRST FORTRAN STATEMENT BELOW DIMENSION STATEMENT IN TEMPSR.	
QVOL	VOLUMETRIC HEAT GENERATION RATE, W/M3(SOLID)	
DELTT	TIME STEP(S)	
DELTZ	DISTANCE BETWEEN AXIAL NODE,M	

OUTPUT VARIABLES: TEMPC BED TEMPERATURE, K COOLANT TEMPERATURE, K TCOLC AT THIS TIME, ALL MATERIALS PROPERTIES ARE ASSUMED COMING THROUGH COMMON BLOCK(S), THESE INCLUDE: ROCOL LIQUID COOLANT DENSITY, KG/M3 ROVAP VAPOR DENSITY, KG/M3 CPCCL LIQUID SPECIFIC HEAT, J/K/KG VAPOR SPECIFIC HEAT, J/K/KG CPVAP LIQUID COOLANT THERMAL CONDUCTIVITY, W/M/K XKCOL VAPOR(STEAM) THERMAL CONDUCTIVITY, W/M/K XKVAP DEBRIS BED DENSITY, KG/M3 RODEB CPDEB DEBRIS BED SPECIFIC HEAT, J/K/KG DEBRIS BED THERMAL CONDUCTIVITY, W/M/K XKDEB ASSUME MATERIALS PROPERTIES ARE TEMPERATURE DEPENDENT, THESE INCLUDE: COOLANT DENSITY, SPECIFIC HEAT, THERMAL CONDUCTIVITY AND DEBRIS BED DENSITY, SPECIFIC HEAT, AND THERMAL CONDUCTIVITY. TEMPERATURES ARE BASED ON OLD TIME STEP VALUES ASSUME ROMX(N2), CPMX(N2), XKMX(N2) ARE KNUWN, FIRST N NUMBERS ARE FOR DEBRIS BED, THE FOLLOWING N VALUES ARE FOR COOLANT. ROZR ROZRC2 . , ROSTR COMMON ROUDZ RCABS , ROCOLD , , , ROCOL CPCOL THELT XMUF 3 X MUCD SURTC ROS AT XKMX XMUCOL XKCOL XLATC RODEB XMUVAP CPDEB CPMX ROVAP XKVAP ROMX HFG TSAT XMUX , , ٠ , , , + , , , , , + . , , , , , + . , CC TEMPCD(20) XMX(40) XKMX(40) AMX(40,40) , TEMPC(20) , RCMX(40) , IPVT(4C) TCOLCO(20) ; BMX(40) ; Z(40) ; , TCOLC(20) , CPMX(40) , DMY(19) DIMENSION , , + , , , 4 , + 000000000 ADJUST CODLANT VELOCITY FROM SUPERFICIAL VELOCITY TO THE TRUE CODLANT VELOCITY IN COOLANT CHANNELS VINCT = VINC / AMAX1(1.0E-8 , POROSC) C 00 150 I = 1 , N2 C 100 J 1 1 , N2 CONTINUE DO 0.0 100

```
C
   150 CONTINUE
C
          DIGUR . HVSC / 2.0 / ( 1.0 - PORDSC )
C
         AMX(1,1) = ROMX(1) + CPMX(1) / DELTT + (XKMX(1) + XKMX(2))
+ 2.0 / DELTZ ** 2 + DIGUR
C
          AMX(1,2) = -( XKMX(1) + XKMX(2) ) / 2.0 / DELTZ ** 2
AMX(1,N+1) = -DIGUR
AMX(N,N-1) = -( XKMX(N) + XKMX(N-1) ) / 2.0 / DELTZ ** 2
C
         AMX(N,N) = ROMX(N) * CPMX(N) / DELTT + (XKMX(N) + XKMX(N-1))
+ / 2.0 / DELTZ ** 2 + DIGUR
C
          AMX(N,N2) = -DIGUR
C
           DIGLL = HVSC / 2.0 / POROSC
C
          AMX(N+1,1) = -DIGLL
C
           AMX(N+1 , N+1) = ROMX(N + 1) * CPMX(N + 1) / DELTT
+ (XKMX(N + 1) * XKMX(N + 2)) / 2.0 / DELTZ ** 2 + DIGLL
ROMX(N + 1) * VINCT * CPMX(N + 1) / 2.0 / DELTZ
C
         AMX (N+1 , N+2) = -(XKMX(N + 1) + XKMX(N + 2)) / 2.0 / DELTZ ** 2
+ ROMX(N + 1) * VINCT * CPMX(N + 1) / 2.0 / DELTZ
C
         AMX(N2 , N2-1) = -(XKMX(N2 - 1) + XKMX(N2)) / 2.0
+ / DELTZ ** 2 - ROMX(N2) * VINCT * CPMX(N2) / 2.0 / DELTZ
C
           AMX(N2 , N2) = ROMX(N2) * CPMX(N2) / DELTT
+ ( XKMX(N2) + XKMX (N2 - 1)) / 2.0 / DELTZ ** 2 + DIGLL
+ ROMX (N2) * CPMX(N2) * VIN:T / 2.0 / DELTZ
C
           AMX (N2,N) = - DIGLL
C
           DC 200 I = 2 , N - 1
C
                  XKUP = (XKMX(I + 1) + XKMX(I)) / 2.0 / 2.0 / DELTZ ** 2
XKDN = (XKMX(I) + XKMX(I - 1)) / 2.0 / 2.0 / DELTZ ** 2
 C
                  AMX(I , I-1) = - XKDN
AMX(I , I) = ROMX(I) * CPMX(I) / DELTT + XKUP + XKDN + DIGUR
AMX(I , I+1) = - XKUP
AMX(I , N+I) = - DIGUR
 C
    200 CONTINUE
 C
           00
                  300 I = N + 2 , N2 - 1
 C
                  XKUP1 = (XKMX(I+1) + XKMX(I)) / 2.0 / 2.0 / DELTZ ** 2
XKCN1 = (XKMX(I) + XKMX(I-1)) / 2.0 / 2.0 / DELTZ ** 2
 C
                  GCDZ = ROMX(I) * VINCT * CPMX(I) / 4.0 / DELTZ
 C
                  AMX(I , I-1) = - XKDN1 - GCD2
AMX(I , I) = ROMX(I) = CPMX(I) / DELTT + XKUP1 + XKDN1 + DIGLL
AMX(I,I+1) = -XKUP1+GCD2
AMX(I , I-N) = - DIGLL
 C
     300 CONTINUE
 C
           DO
                400 I = 1 , N
 C
                  XMX(I) = TEMPCO(I)
```

TABLE A-16. LISTING OF DBDRIV

```
C
    400 CONTINUE
C
            DO 500 I . N + 1 , N2
C
                   XMX(I) = TCOLCO(I-N)
C
    500 CONTINUE
C
                   600 I = 1 , N2
BMX(I) = 0.0
            DO
C
                           700 J . 1 , N2
CST . AMX(I,J) * XMX(J)
BMX(I) = BMX(I) + CS
                    DG
    700
                   CONTINUE
C
    600 CONTINUE
С
            \begin{array}{rcl} & \texttt{BMX(1)} & \texttt{BMX(1)} & \texttt{OVDL} & \texttt{2.0} & \texttt{HTLBCD} & \texttt{DELTZ} \\ & \texttt{BMX(N)} & \texttt{BMX(N)} & \texttt{OVDL} & \texttt{2.0} & \texttt{HTUBCD} & \texttt{DELTZ} \\ & \texttt{BMX(N+1)} & \texttt{BMX(N+1)} & \texttt{2.0} & \texttt{HTLBCC} & \texttt{DELTZ} \\ & \texttt{BMX(N+2)} & \texttt{BMX(N+1)} & \texttt{2.0} & \texttt{HTLBCC} & \texttt{DELTZ} \\ & \texttt{BMX(N2)} & \texttt{BMX(N2)} & \texttt{2.0} & \texttt{HTUBCC} & \texttt{DELTZ} \end{array}
C
            DO
                   800
                           I=2,N-1
C
                   BMX(I) = BMX(I) + QUCL
¢
    800 CONTINUE
C
Ĉ
            ADJUST TEMPSR FOR LOW GVOL AND LOW HTUBC AND HTLBC SITUATIONS.
                                  .AND. HTUBCD .LT. 1.CE-05
.AND. HTUBCD .LT. 1.OE-05 )
                    ( QVOL
            IF
          ٠
                                                                                                         THEN
С
                   00
                          750 I = 1 , N2
C
                            IF ( I .LE. N )
XADJ = DIGUR
AM (I,I+N) =
                                                               THEN
                                                            AMX(I, I+N) - DIGUR
C
                            EL SE
                                    XADJ - DIGLL
AMX(I,I-N) - AMX(I,I-N) - DIGLL
C
                            ENDIF
C
                            AMX(I,I) = AMX(I,I) + XADJ
BMX(I) = ROMX(I) + CPMX(I) + XMX(I) / DELTT
¢
    750
                   CONTINUE
C
            ENDIF
000
            NOW SOLVE AMX(N2,N2) * XMX(N2) = BMX(N2) FOR XMX(N2)
                     LSGECD
                                                                                           RCOND , Z
BMX , O )
                                          AMX , N2 , N2 , IPVT ,
            CALL
                                                                                                               )
C
            DO 900 I=1,N
C
                    TEMPC(I) = BMX(I)
TCOLC(I) = BMX(N+I)
C
    900 CONTINUE
C
            RETURN
            END
```

* PROGRAM DBDRIV SUBCODE NAME: DBDRIV PURPOSE: DRIVER FOR OBFRAG, DBFROZ AND ASSOCIATED ROUTINES WHICH SIMULATES DBUNDL IN TESTING AND INITIAL INTEGRATION PHASES CALLING SUBROUTINES: NONE SUBROUTINES CALLED: DEBINP , DBTIME , DBFRAG , CBFROZ , DBOUTD WORK PACKAGE: 15 ENGINEER/PROGRAMMER: S.T.HSIEH/G.H.BEERS LALT MODIFICATION DATE: 11/30/81 IN DBUNDL SUBROUTINE, ALL OF THE FOLLOWING VARIABLES WILL BE IN ADJUSTABLE ARRAYS, WITH DIMENSIONS VARYING WITH THE NUMBER OF NODES AND DEBRIS REGIONS. IMPLICIT INTEGER (I - N) CC BEDTMR ELVAY IMT XMUX FRAG ESTDT COLTMR BED TMP ROMX XKMX FROZEN CURTIM ELVAR IRT COLTMP CPMX DIMENSION ~~~ 4144000 4444200 4444000)))) \$ -----""))))))))))))) ,,,, , , + , , ++ () , ,)) , , , RBDRPT ٠ ٤ cc RDZR XMUCD SURTC RDSAT XKMX ROZRO2 ROCOL CPCOL TMELT XMUF3 ROUO2 XMUCOL XKCOL XLATC RODEB ROCOLD HEG TSAT XMUX ROSTR ROVAP XKVAP ROMX ROABS XMUVAP CPDEB CPMX COMMON , , , , , , + , , , , , , ٠ , , , , , , ٠ , , , . . ٠ . , cc LOGICAL FRAG , FROZEN , REDRPT 000000 CALL *DEBINP* WHICH WILL DEFINE I/O VARIABLES NEEDED IN TESTING CALL DEBINP XMA SSR ABSMR ZRD2TR HTLBRD IDREGR BEDTMR ZRMC ZRMR AREAR ZROZAR HTLBRC NONR OXDAR ZROZMC SIZAVR STRMR VINR ELVNR * * * ZRD2MR HITRG ALPHTR HTUBRD UD2MR VINROD ALPHAR HTUBRC + (", ; ; , ٠ , + , , , + , , , , , MAXL COLTMR XMASSC EL VAR IRT FISHR UD2MC +++ ,,, , , , , , , , , ٠ , . , .

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ABSMC
ZRD2AC
HTLBCC
ELVAY
FISHC
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ALPHTC
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BEDTMP
ELVMC
FROZEN
                                                                                VINC
ALPHAC
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COLTMP
ND
RBORPT
                                                                                                VINCOL
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   DETERMINE DISRUPTED TIME ARRAY
           CALL DETIME ( T , N )
C
           I = 1
Ċ
      10 CONTINUE
0000
    IF I IS LESS THAN N, THEN ITERATE AGAIN INCREASING TIME STEP
           IF ( I .LE. N )
                                             THEN
CCC
    DETERMINE CURRENT TIME STEP
                  DELTT - T ( I + 1 ) - T ( I )
CCC
    ITERATE ON K UNTIL ALL REGION'S BEHAVIOR HAVE BEEN DESCRIBED
                  00 100 K = 1 , NUMREG
0000
    COMPUTE FRAGMENTED DEBRIS BEHAVIOR FOR REGION K IF FRAG(K) = TRUE
                          IF ( FRAG (K) ) THEN
000000
    MAKE THE CALL
RUBBLE DEBRIS
                             TO DEFRAG, THE DRIVER WHICH WILL HANDLE THE BEHAVIOR
                                        DBFRAG
SIZAVR
STRMR
VINR
ELVNR
IRT
POROPR
VELMOT
RBORPT
                                 CALL
                                                        XMASSR
ABSMR
ZRD2TR
HTLBRD
MAXL
ELVAR
DXDAR
XCHRL
T
                                                                                          ZRC2MR
HITRG
ALPHTR
HTUBRD
IDREGRR
HITER
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, VINROD
, ALPHAR
, HTUBRC
, NONR
, THMOTR
, PGROSR
, DOWNR
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AREAR
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CC
           PRINT
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C 10	CONTINUE	YCHRL , EFFDIA , KTERMC , IDREGN , NOND ELVAY , BEDTMP ; COLTMP ; IMT ELVMC , DOWNZ , VELMTC ; CURTING K) DELTT , FRAG(K) , FROZEN(K) ;
c	I • I + 1	
c c	ENDIF	
č	END	



TABLE A-17. LISTING OF DEBINP

	+++++++++++++++++++++++++++++++++++++++		BF		U	T :	IN	E	D	E	B	IN	P			SAVERCXANTERF	LTILADABRILVSA	AMANLISMNBAHG	VR R MSCACYC	a 000 000	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	XANTHONTATOUL	TORTOURH LTWLY	ASOLRDATPUDVO	SREAGE CHOMON	Z DOG DADA Z	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,		ZARTOXRILICOB	C LCSZOZLOWI	RAZBRAZCHET R	RC CCP T			ZHAHIFUVEIINC	RIFUTSZNVRT	NRIB ILOZU L	MGTR RCOCG	R RD D 7 1	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	TO THIS WATER	DILTLITRTOXU	ZNPUVVROLNOM	ROARRETC	DRC CD G	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,
SUB PUR SUBRUS ELAS	CP LRKIT	DS ZUPER	EE GTAED	N SNK	A DEAPE	MISBSGRI	ENADO -GA	PUUART		EATNESTN	BRUND H	IN SSI	PIO	NUN	UPON .	TUDET	5 .H	151	BR	EH I	U 1	G.	H T	ER .	BE	0 ,	RD	00	BR L	RG	A	A	AND	D	M	DE	FP	RR	gz	R	đt	H	CN	s		
THE BEAT RHE FUE	SAAT	SIWNCB	UCILICU	R L PD		UCCI	TOPNOG	NLETEE	E	HRRNME	NIUST	INMUTR	HRHRZ .	ALSNSG	1*10	NOHNO	EBALOR	R	T A	HGPPD	ULUB	INN .IH	PONA	U OPY		A AGO	ARNHM	A0 . L0	Z DOE	E BAL	RET	EIGA	OZZIZ	BS	YCIATHI	TADA	HP TB	E M	ALS	EDPED	BORD	FIN	STEL	HI B	s 1-	•2
IN	*I G T	DEAL	BLG	IN	POU	* IR	MEPO	LINS	LSI	V	ANC	RI	A) Y	81	ET	SH		I	TS	HPE	C	HE	T	E	xc	E	PT	IN		в	OF	. ~	TH	E	01	REB	GR	I	S	R	FL	A 1	GS	is	AR	EOR
***	*	•1	NI	PU	T		AN	10	0	10	Т	PL	т	۱	/ A	R	IA	B	L	ES	,	AN	0	1	Тн	E	IR		DE	s	CF	11	PT	1		is	*	•	• •	**	•					
SEE	P	TH	F	=	EV	A	RI	A	BL	E	н	DE	S		RI	MP		EC	LZ	s.	F	IN	A	L	0	E	SI	G	N	R	EP	0	RT		B	r	S	•	T	•	ł	15	IE	H	F	OR
		IM	PI	LI	c	I	T		IM	11	E	GE	R		(I	-	à	N)																									
ĉ	•	DI	ME	N	s	I		•				and of	LRO	¥"	AR	P			444	1	~~~			BIE	EV	TA	MR		~~~~	444	1	~~~~			CIBR		TTX	MI	RP		44.4	1			,,,	

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XMUX FRAG CURTIM CPMX 4000 444 40 20 20 KMX (FROZEN (40) >>>> ンシン ; 1 * . . ٠ , ٠ (RBORPT + CC ROZR XMUCD SURTC ROSAT XKMX ROZRO2 ROCOL CPCOL TMELT XMUF3 R DUU2 XMUCOL XKCOL XLATC R DDEB RD ABS XMUVAP CPDEB CPMX ROCOLD , HEG , TSAT , XMUX , ROS TR ROVAP XKVAP RUMX , , , , COMMON , , , , ... ; ,, , ٠ + ٠ , , , . , ٠ , CC FRAG , FROZEN , RBORPT LOGICAL 000000 DEFINE THE NUMBER OF NODES, REGIONS, AND TIMESTEPS. NUMPEG · 20 N 0000 INITIALIZE REGION DEBRIS TYPE FLAGS FRAG 1 12)) : C FROZEN : .FALSE. " 1 12 0000 INITIALIZE DISRUPTION FLAGS FOR ALL REGIONS DO 5 K = 1 , NUMREG C RBDRPT(K) = .FALSE. Ç 5 CONTINUE CCCCC DEFINE MATERIAL PROPERTIES FOUND IN COMMON BLOCK ROZR ROZRO2 ROUD2 ROSTR ROABS ROCOL XMUCOL ROVAP XMUVAP 6.552E+03 5.82E+03 1.097E+04 8.0E+03 488.418 8.68E-05 160.20 1.255E-05 : ٠ .

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HSDPCCAPB
HSDPCCAPB
TRODAB
TRODACATT
TRODACATT
TALODA
                                                                                                                         1.661E+06
59.3E+03
3.683E+04
3.2093E-01
5.80.0
700.0
480.418
3150.0
2.74E+05
8.62E+03
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CPMX
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C
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                                                                                    XMUX
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C
                                                                                     XKMX ( I ) . 1.904
XKMX ( I + ND ) = XKCOL
Ç
                           20 CONTINUE
 000000
                 DEFINE DATA THAT WILL BE INPUT BY DUMMY ARGUMENTS. THIS GROUP
CONTAINS INPUT FOR FOCHAR, A FEW OF WHICH ARE ALSO INPUT TO FROZTH.
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 CCC
                   THIS GROUP
                                                                                                        OF VARIABLE DEFINITIONS CONTAINS INPUT FOR FRAGTH
                                                    ZRCZTR
ZRCZAR
ALPHTR
ALPHAR
                                                                                                                            0.5E-06
0.5E-10
0.5E-06
0.5E-10
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2.5
ELVNR + HITRG
0.0
0.0
C.0
C.0
41
        ELVNR
HTLBRD
HTLBRC
HTUBRC
HTUBRC
MAXL
                   ......
000
   THESE OUTPUT VARIABLES MUST ALSO BE INITIALIZED
         IDREGR = 1
NONR = 20
0000
   INITIALIZE ELEMENTS 1 TO NONR OF THESE ARRAYS
         DIV
                   = FLOAT ( ND - 1 )
c
         00
               40
                  I = 1 , NONR
C
               FACTOR = ( I - 1 ) / DIV
C
               IRT (
ELVAR
COLTMR
BEDTMR
                                     0
ELVNR + 0.2 *
430.0 + 190.0
COLTMR ( 1 )
                                  ....
                        I
                          )
                         100
                            I
                                                         FACTOR
FACTOR
                               }
C
    40 CONTINUE
C
         DXDAR
                   1.69E+08
1.69E+08
00000000
   NOW SET UP THE INPUT VALUES FOR FROZEN BEHAVIOF
                      ..............
                                 HITEC
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IDREGN . 5
NCNO . 22
000
   INITIALIZE FIRST 2 ELEMENTS OF FOLLOWING OUTPUT ARRAYS
                                        0
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2.55
670.0
670.0
670.0
           IMT (
IMT (
ELVAY
COLTMP
BEOTMP
BEOTMP
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                       よろして
                                     .
                                     .
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                                     .
                             NUNI
                                     ....
                                 .
0000
    INITIALIZE ELEMENTS 3 THRU NOND OF THE ABOVE CUTPUT ARRAYS
           DO 60 I = 3 , NOND
c
                   FACTOR = ( I - 3 ) / DIV
C
                                                0
2.6 + 0.
680.0 +
COLTMP
                   IMT ( I )
ELVAY ( I
COLIMP (
BEDIMP (
                                    )
I
I
                                             ....
                                                            0.4 * FACTOR
+ 190.0 * FACTOR
( I ) * FACTOR
                                         ))
C
      60 CONTINUE
CCC
    ASSIGN VALUES TO DATA IN FRCHAR ARGUMENT LIST
           XMASSC = 1.3122E-01 * 264.0
ZRMC = 1.99556E-02 * 264.0
ZR02MC = 1.419E-03 * 264.0
U02MC = 1.09844E-01 * 264.0
STRMC = 0.0
ABSMC = 0.0
AREAR = 3.664E-02
VINCOD = 5.05
C
            RETURN
```

TABLE A-18. LISTING OF DBTIME

SUBROUTINE OBTIME (TIME , N) THIS IS A DUMMY SUBROUTINE WHICH WILL CALCULATE THE TIME INTERVALS FOR THE DISRUPTED BUNDLE LOGIC. DIMENSION TIME (N + 1) C DELTAT = 10.0 DO 20 I = 1 , N + 1 TIME (I) = FLOAT (I = 1) * DELTAT C CONTINUE RETURN END TABLE A-19. LISTING OF DBOUTD

		*******	su	8 F	10	U	21	IN	E		DI	80	UT	0		TXOUYUUUU	ITOLCLLE	TELVHVVL	RMMRLYCA	R		,,,,,,,,	PHHEEBOR	DORSHUDR	RRTTFDWA		RR			PATHKOVE	DOHITCHER	CROBRENZ	PTCMMTE	R R CACZ	,,,,,,,)		XEDPIIC	HVWRRTR	RANDET	LRRSG H		******	HZ DC DX	FUUDOI	UTMODO	I DR TC	
000000000	SUBPUR	CPLRK	DSNUP	ELGTAL	Z SZK	A DHAD	MTBSGO	E	PUAD	RILLI	BZZUN		Ŧ	DHOA	800		a	R	15		B	EH	A	V	10		2	Al	A	L	YS	5 1	s			T	PI	JT									
CCC C	LAS	ŝŧ	M	01	D'I	F	Î	CA	Î	îc	N	ĉ	A	1 5	:	• •	i	1	1	30	7	81			•	00	-	n.,	,																		
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00000	* DB SIM TES	STE	LA	DIGI	IN NO	IGF	s u	*1 *1	UBB	RR	EDAH	NILGE	V	AHAN	I	NCHE	TDO	HWOL	EASFI	F	UNZE	RR *	DE	TITB	EHR	RENE	0-0	DOUR	IRP PG	EEUI	DRTO	A Can	RIT	MLY	TH	ELB	EEF	DRAPALA	LCRG	VI I I	HUNZR	TED	RORR			NE	
c		:	01	M	EN	15	I	01	4				ELC	RID	T	R	>	(444		>>>	, , ,		BELL	EDLY	TA	MI	R	""		4141		~~~	, ,		CB	e	Ţ	M	RP	(44	1	>>	;	
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c			w R W R	I	TE TE	(6	;	10	060)		DELHES	OBRAT		R	R(RI,	E C		- NIN	R	IY,	PE	,E	FILM	RCO	NAR		NO)	S) 1 V M	R	то ,	1	101	NR	• ,
c		ELSE	I	F	(F	ROZ	EN	1)	1	THE	N																									
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			NR.	1	TE	(6	,	1	050)		:8	EEE		Î	EM	PE	R	AŢ	U	RÊ	;		÷ ,	1				10	΄,						
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