

CAUSTIC FEED DESIGN ANALYSIS
DESIGN CHANGE 77-9
CONTAINMENT SPRAY SYSTEM MODIFICATION
SURRY POWER STATION- UNIT 2

THIS DOCUMENT CONTAINS
POOR QUALITY PAGES

8006190 550 XA

INTRODUCTION

The Containment Spray System of Surry Unit No. 2 has been modified in order to provide assurance of meeting site boundary dose limitations set forth in 10CFR part 100. These modifications involved modifications to the caustic addition system and the installation of a new spray ring header within containment along with other related changes. This report involves itself with analyzing the performance of the modified caustic addition system which with the other containment spray modifications will be capable of meeting parameters of spray pH and sump pH.

Part A demonstrates maximum and minimum spray and sump pH values versus time based on calculated data for twelve (12) scenarios utilizing different combinations of two (2) containment spray and four (4) safety injection pumps. As shown by these curves, the spray pH remains within the bounds of 8.5 to 11.0 set forth in the Standard Review Plan 6.5.2. In addition, the ultimate sump pH value is 8.2 which will enable the Recirculation Spray System to remove atmospheric radioactive iodine and prevent it from leaving the sump solution for long term considerations.

Part B of this analysis deals with the determination of Caustic Fluid Flow Rate History (CFFRH) which is derived from calculated head loss values of the caustic addition piping system and Caustic Addition Tank levels for the twelve scenarios discussed in Part A. Two (2) major considerations used during calculations flow rates were:

1. Is a restrictive flow orifice required; and if so, it must be designed to meet flow requirements which yield caustic for a spray pH range of 8.5 - 11.0 for all pumping scenarios.
2. The Caustic Addition Tank must empty completely during each of the pumping scenarios in order to take credit for the entire tank volume for ultimate sump pH considerations.

As shown by the curves of caustic flow for the twelve scenarios, the flow rate in all cases remains within the bounds of a maximum and minimum rate which would result in a spray pH of 8.5 to 11.0.

In conclusion, the new system for caustic addition will be a reliable means of adding sodium hydroxide solution to the containment spray fluid which will provide iodine removal and consequently keep site boundary dose within the limits of 10CFR part 100.

PART A

PART A

CONTAINMENT SPRAY SYSTEM - SURRY #2 SPRAY AND SUMP pH vs. TIME HISTORIES

Figures 1-12 demonstrate that spray pH is maintained between 8.5 and 11 during each of twelve(12) scenarios utilizing combinations of four pumps for the following considerations following a design basis accident. The values of spray pH shown in these curves were developed from caustic flow histories presented in Part B. The documents from which these curves are taken are filed under Stone & Webster calculation numbers 12846.07-35 and 57 and 12846.07-PE-037-0.

- Figures 1-4 Starting parameters in these scenarios will maximize spray pH. (10.75 maximum scenario No. 4)
- Figures 5-8 Starting parameters in these scenarios will minimize spray pH. (9.0 minimum, scenario No. 8)
- Figures 9-12 Starting parameters are used which will maximize the time required to empty the caustic addition tank. Relating to the minimum time to empty for the RWST. (3860 sec. CAT vs 3975 RWST, scenario No. 11)

Figure 13 shows sump pH vs. time history after LOCA. This curve, developed from scenario 11, postulates the longest emptying time for the CAT relative to the RWST. As shown by this curve, ultimate sump pH will be 8.2.

APPENDIX A

SCENARIO NO.1 ICS PUMP + IHST + IHST WITH MAX SPRAY pH ASSUMPTIONS

Orifice $H_L = 1350 \times 10^{-6} \text{ Ft/CPM}^2$ (+)

Orifice $H_L = 1800 \times 10^{-6} \text{ Ft/CPM}^2$ (x)

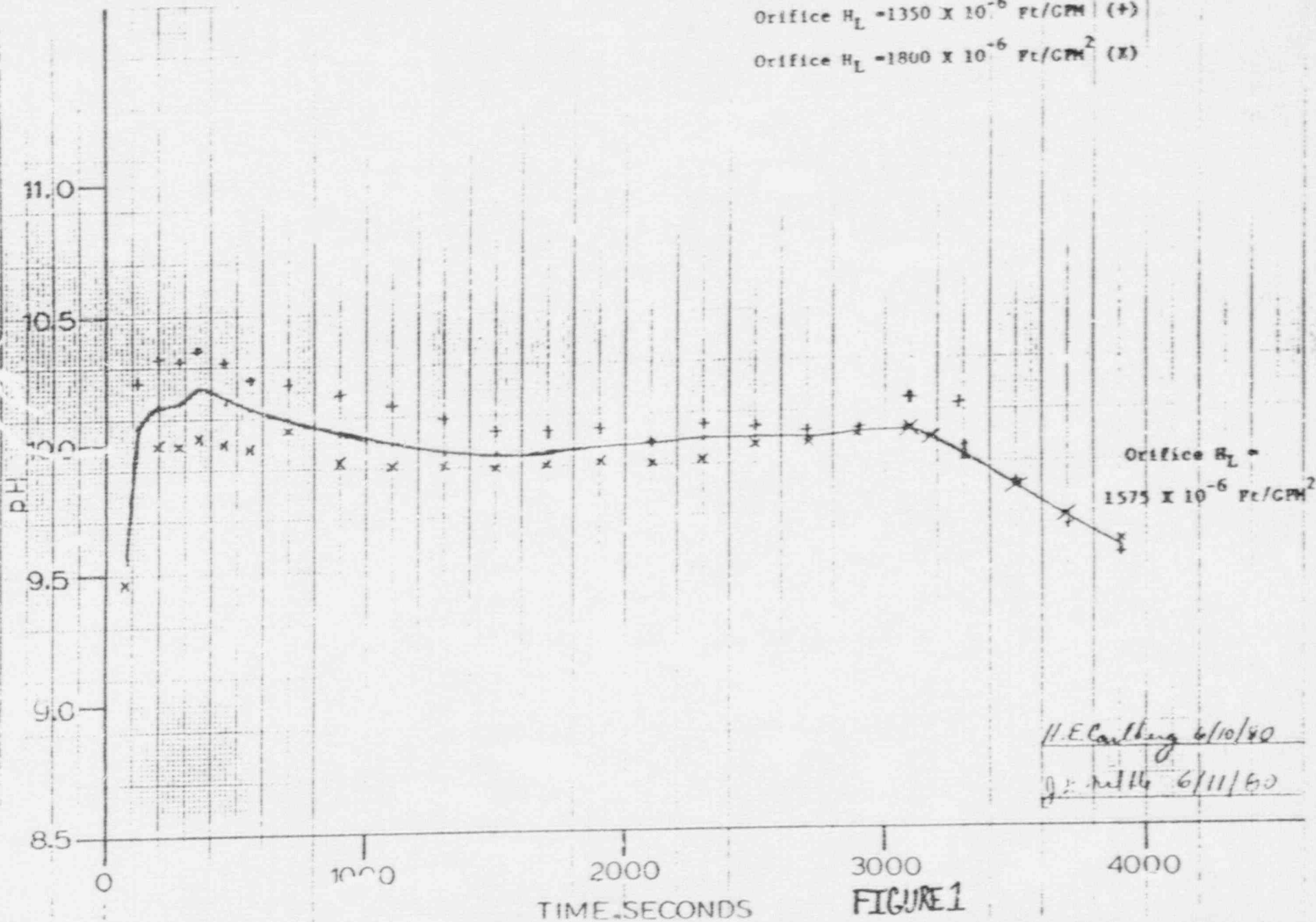


FIGURE 1

APPENDIX A
SCENARIO NO. 2 2 CS PUMPS + 2 LHSI + 2 HHSI WITH MAX SPRAY PH ASSUMPTIONS

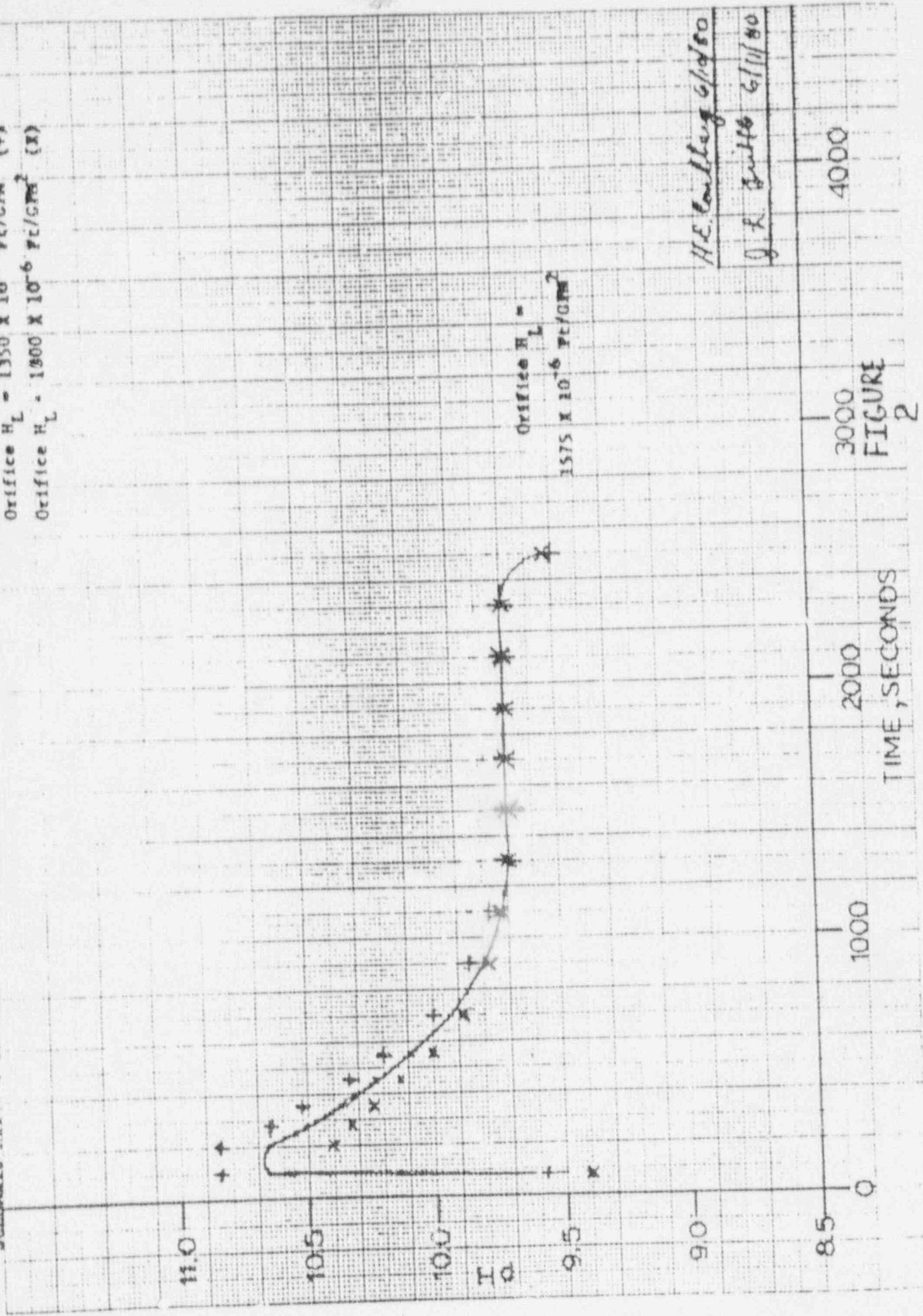
Orifice $H_L = 1350 \times 10^{-6} \text{ Ft/CFM}^2 (+)$

Orifice $H_L = 1800 \times 10^{-6} \text{ Ft/CFM}^2 (X)$

Orifice $H_L = 1575 \times 10^{-6} \text{ Ft/CFM}^2$

H.E. Cantley 6/1/80

J.R. Smith 6/11/80



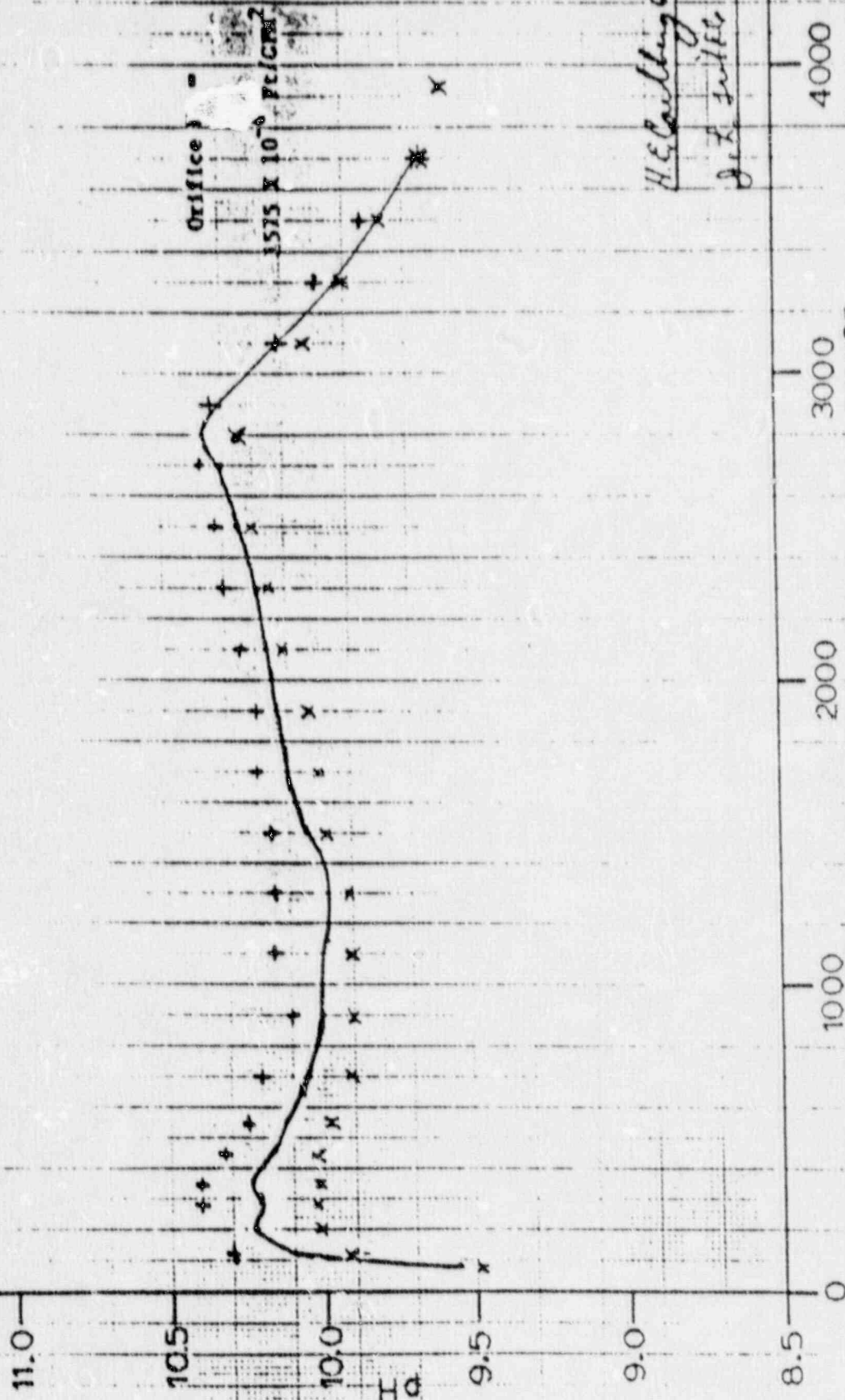
3000
4000
FIGURE
2

TIME, SECONDS

APPENDIX A
 SCENARIO NO. 3 1CS PUMP + 2 LHSI + 2 RHHSI WITH MAX SPRAY PH ASSUMPTIONS

Orifice $H_L = 1350 \times 10^{-6} \text{ Ft/GPM}^2 (+)$

Orifice $H_L = 1200 \times 10^{-6} \text{ Ft/GPM}^2 (X)$



H.C. Carling 6/19/80
 J. L. Miller 6/17/80

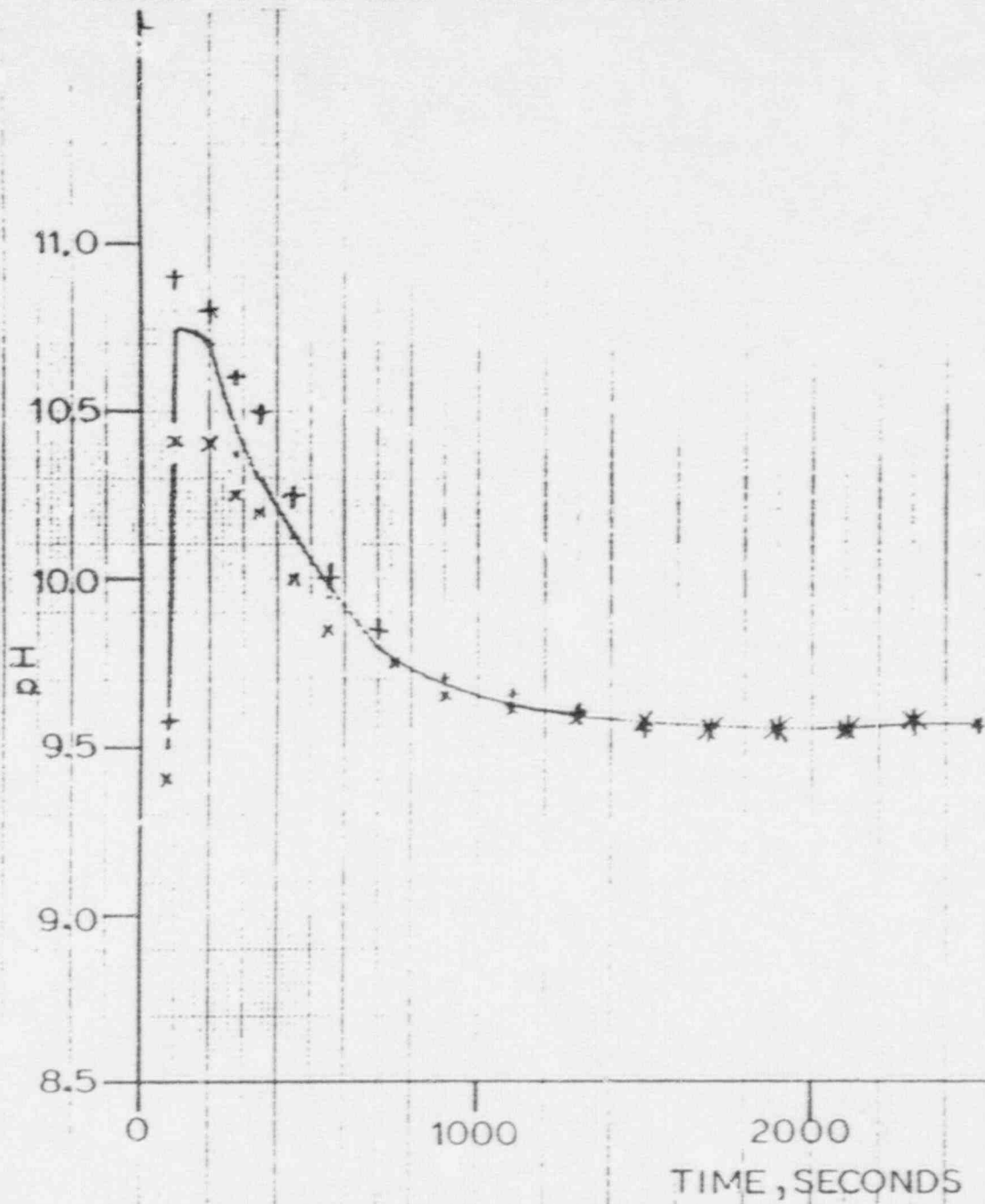
FIGURE 3

APPENDIX A

SCENARIO NO. 4: 2CS PUMPS + 1 LHSI + 1 HHSI WITH MAX SPRAY pH ASSUMPTIONS

Orifice $H_L = 1350 \times 10^{-6} \text{ Ft/GPM}^2 (+)$

Orifice $H_L = 1800 \times 10^{-6} \text{ Ft/GPM}^2 (x)$



Orifice $H_L = 1575 \times 10^{-6} \text{ Ft/GPM}^2$

H.C. Co. 1/20/80
J. F. Public 5/11/00

FIGURE 4

APPENDIX A
 SCENARIO NO. 5: 1 CS PUMP + 1 LHSI + 1 HHSI WITH MIN SPRAY PH ASSUMPTIONS

Orifice $H_L = 1350 \times 10^{-6} F_t / \text{GPM}^2$ (+)

Orifice $H_L = 1800 \times 10^{-6} F_t / \text{GPM}^2$ (x)

11.0

10.5

10.0

H_L

9.5

9.0

8.5

Orifice $H_L =$
 $1575 \times 10^{-6} F_t / \text{GPM}^2$

H.E. Carlsberg 6/10/80
J. J. Smith (111)

1000

2000

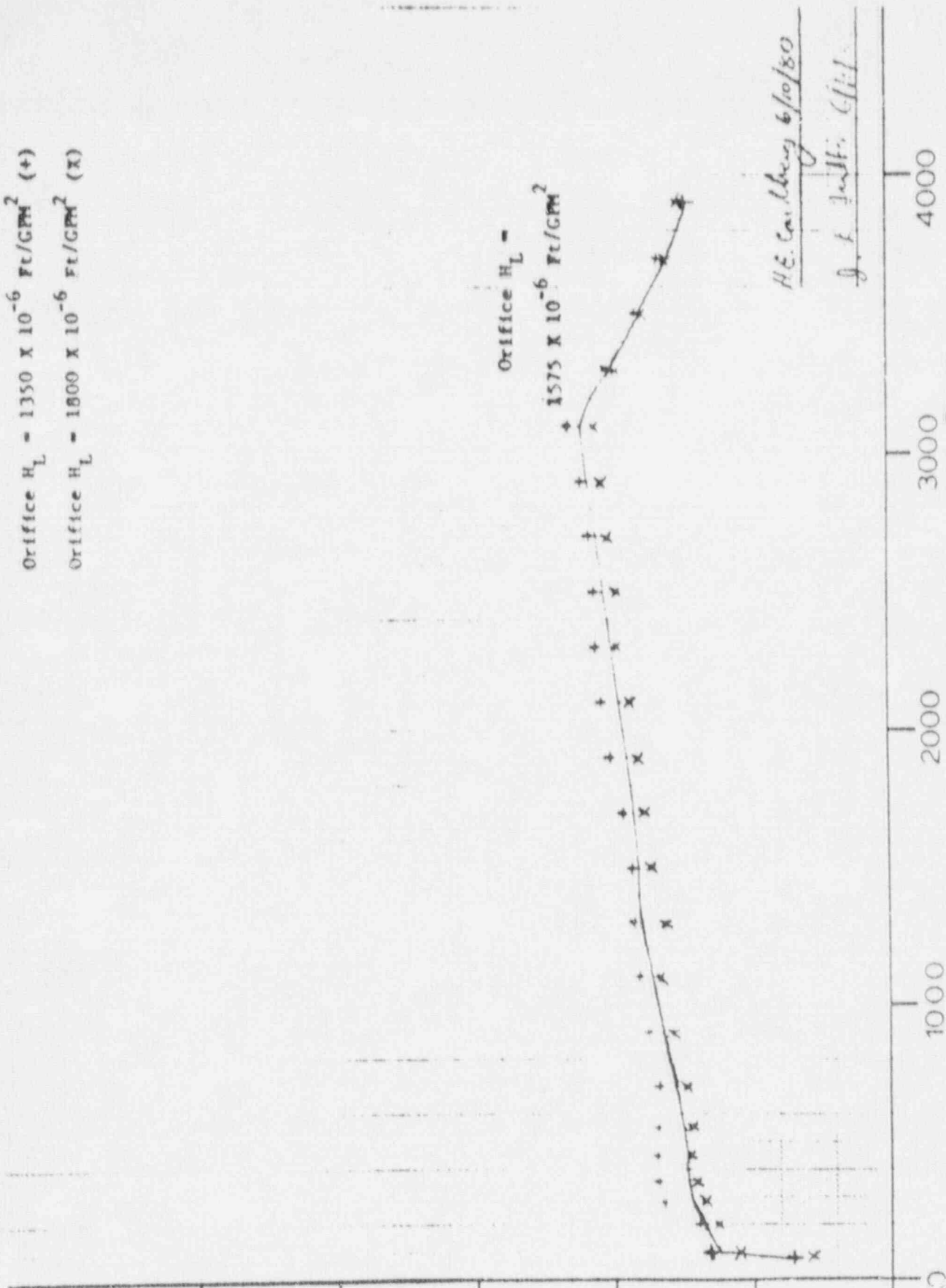
3000

4000

FIGURE

5

TIME, SECONDS



APPENDIX A
 SCENARIO NO. 6: 2 CS PUMPS + 2 LHSI + 2 HHSI WITH MIN. SPRAY pH ASSUMPTIONS

Orifice $H_L = 1350 \times 10^{-6} \text{ ft/GPM}^2 (+)$

Orifice $H_L = 1800 \times 10^{-6} \text{ ft/GPM}^2 (X)$

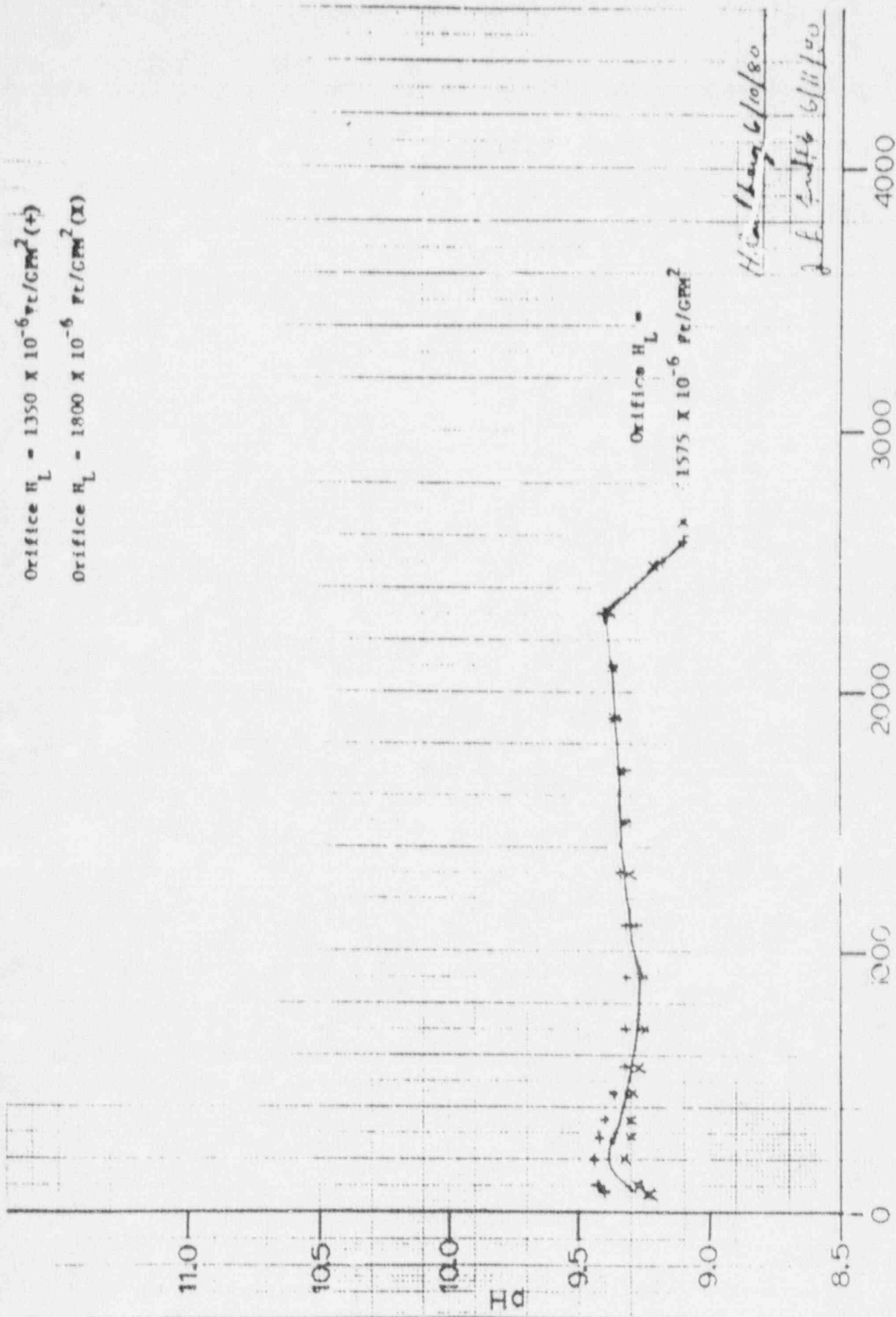


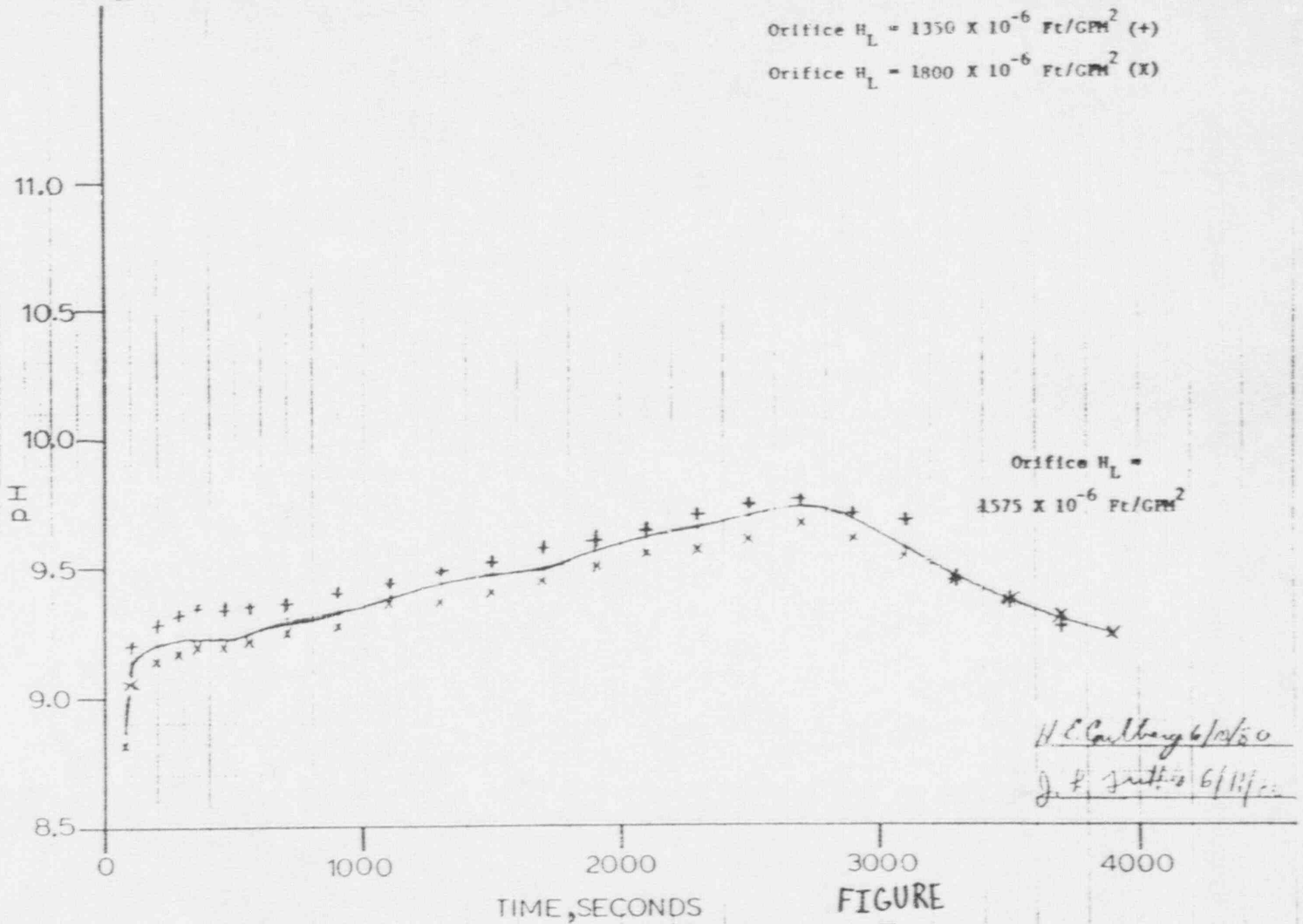
FIGURE 6

APPENDIX A

SCENARIO NO. 7: 1 CS PUMP + 2 LHST + 2 HHSI WITH MIN SPRAY pH ASSUMPTIONS

Orifice $H_L = 1350 \times 10^{-6} \text{ Ft/GPM}^2 (+)$

Orifice $H_L = 1800 \times 10^{-6} \text{ Ft/GPM}^2 (x)$

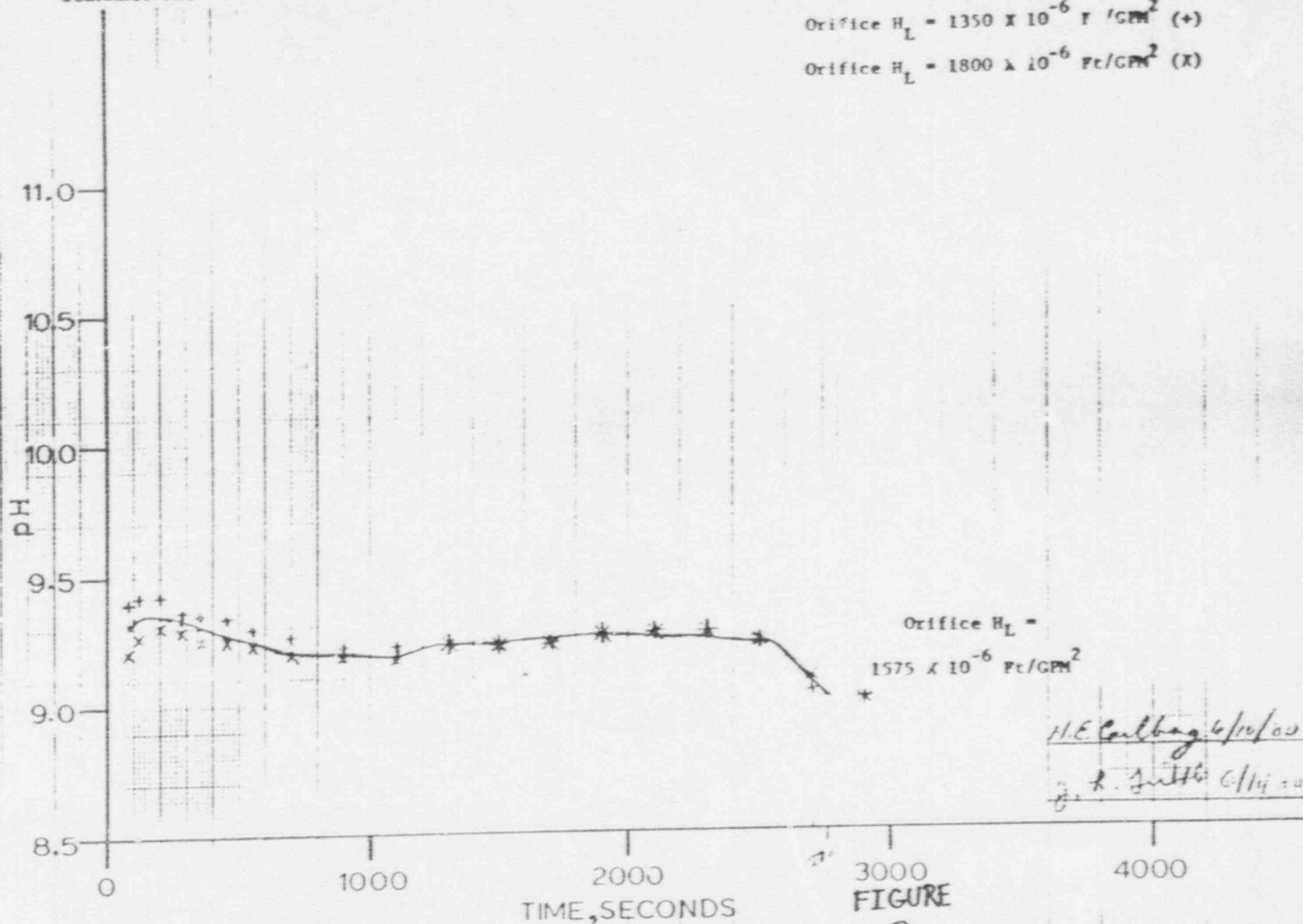


APPENDIX A

SCENARIO NO. 8: 2 CS PUMPS + 1 LHSI + 1 HHSI WITH MIN SPRAY pH ASSUMPTIONS

Orifice $H_L = 1350 \times 10^{-6} \text{ Ft/GPM}^2 (+)$

Orifice $H_L = 1800 \times 10^{-6} \text{ Ft/GPM}^2 (X)$



Orifice $H_L = 1575 \times 10^{-6} \text{ Ft/GPM}^2$

H.E. Carlberg 6/10/00
R. J. Little 6/11/00

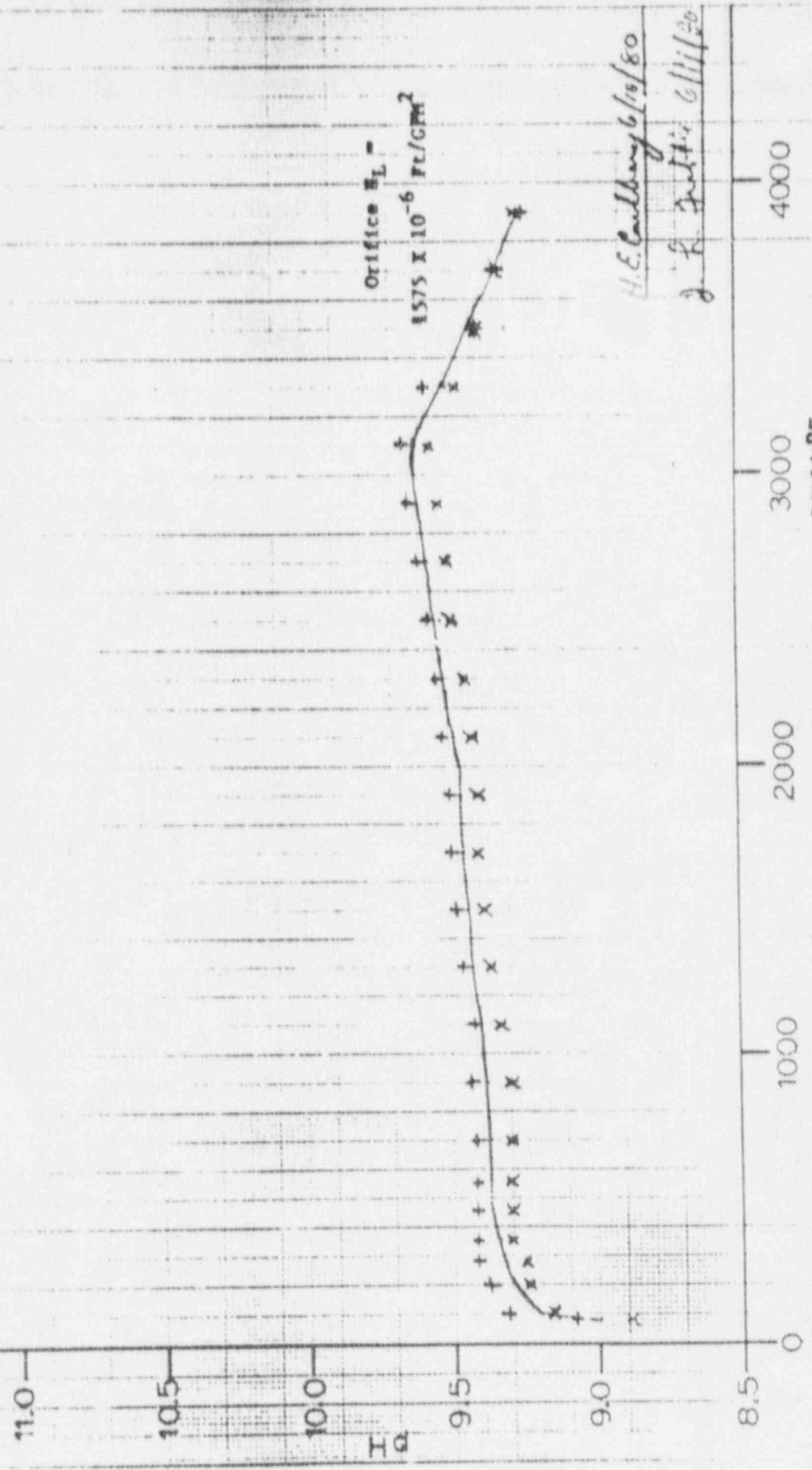
FIGURE 8

APPENDIX A
 SCENARIO NO. 9: 1CS PUMP + 1 LUSI + 1 HHSI WITH MIN SUMP PH ASSUMPTIONS

Orifice $H_L = 1350 \times 10^{-6} \text{ Ft/GPM}^2$ (+)

Orifice $H_b = 1800 \times 10^{-6} \text{ Ft/GPM}^2$ (x)

Orifice $H_L = 1575 \times 10^{-6} \text{ Ft/GPM}^2$



H. E. Carlsberg 6/10/80
 J. R. Dutton 6/11/80

FIGURE 9

APPENDIX A
 SCENARIO NO. 10: 2 CS PUMPS + 2 LHSI + 2 RHSI WITH MIN SUMP pH ASSUMPTIONS

Orifice $H_L = 1350 \times 10^{-6} \text{ FT/GPM}^2$ (+)

Orifice $H_L = 1800 \times 10^{-6} \text{ FT/GPM}^2$ (X)

11.0

10.5

10.0

H_p

9.5

9.0

8.5

Orifice $H_L = 1575 \times 10^{-6} \text{ FT/GPM}^2$

H.E. Carlsberg 6/10/80

J. P. G... 6/11/80

1000

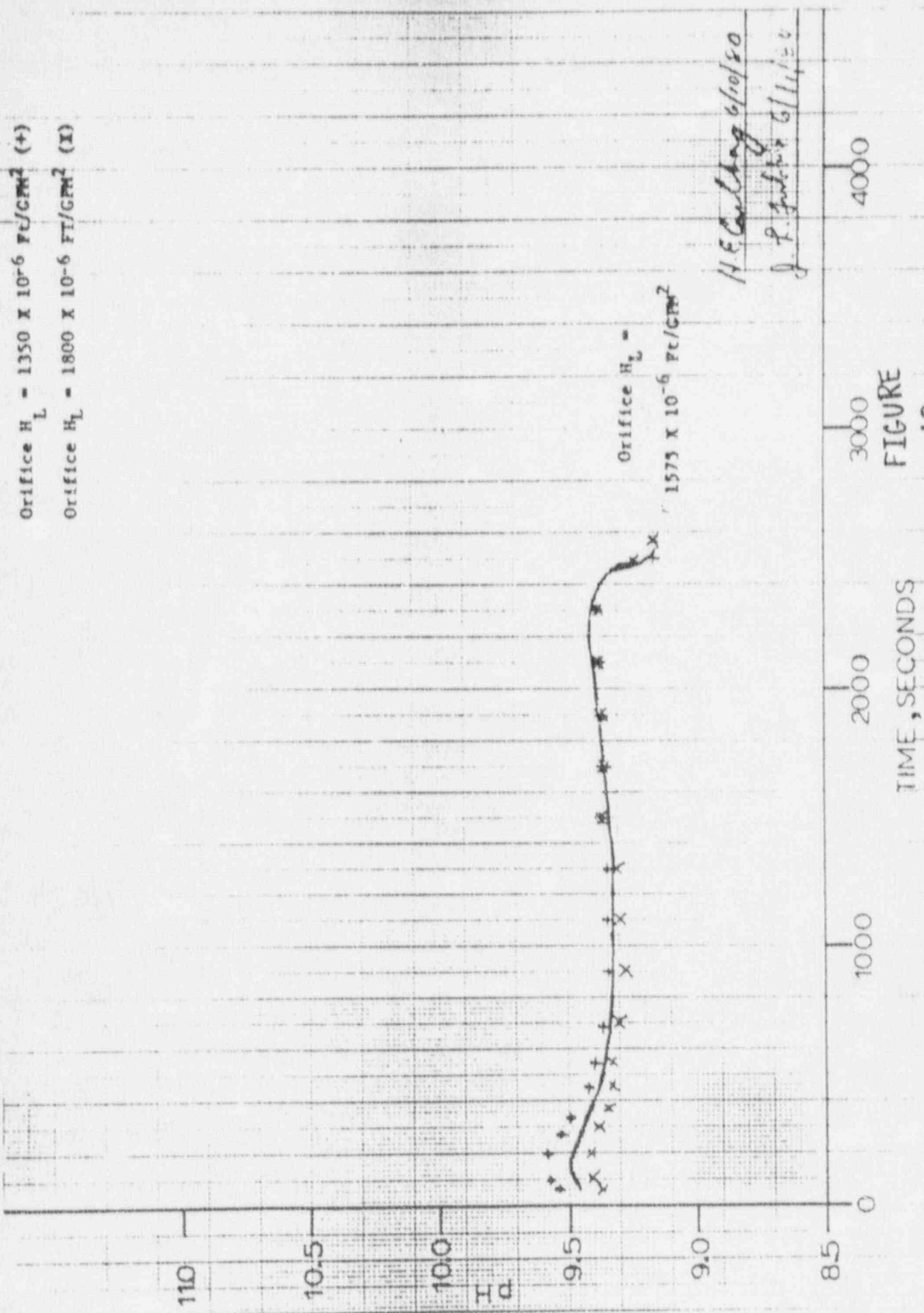
2000

3000

4000

TIME, SECONDS

FIGURE 10



APPENDIX A
 SCENARIO NO. 11: 1 CS PUMP + 2 LHSI + 2 HHSI WITH MIN SUMP PH ASSUMPTIONS

Orifice $H_L = 1350 \times 10^{-6} \text{ Ft/GPM}^2$ (+)

Orifice $H_L = 1800 \times 10^{-6} \text{ Ft/GPM}^2$ (x)

Orifice $H_L = 1575 \times 10^{-6} \text{ Ft/GPM}^2$

H.S. Galloway 6/10/80
J. L. Fisher 6/11/80

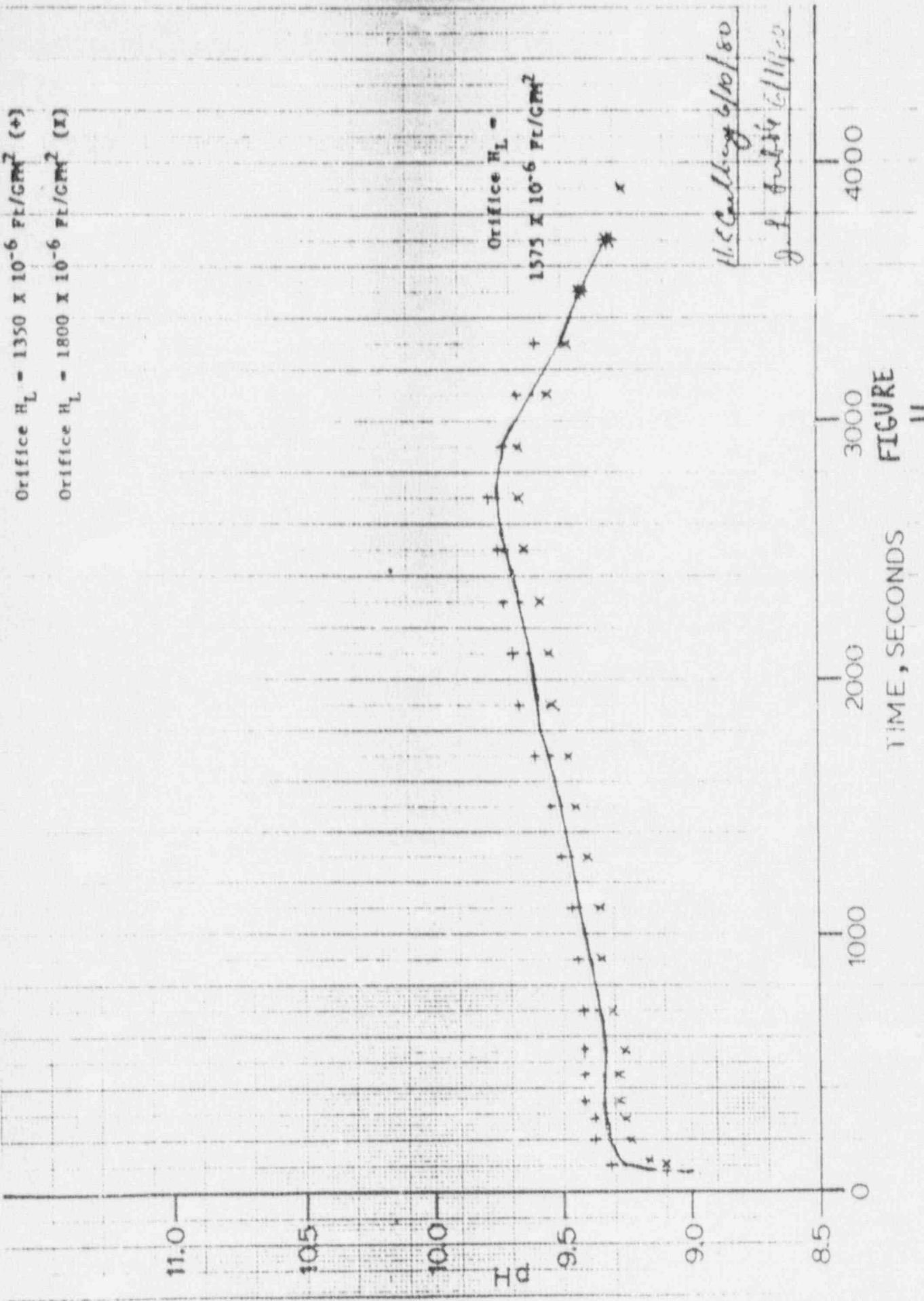


FIGURE II

TIME, SECONDS

APPENDIX A
SCENARIO NO. 12: 2 CS PUMPS + 1 LHSI + 1 HRSI WITH MIN SUMP PH ASSUMPTIONS

Orifice $H_L = 1350 \times 10^{-6} \text{ Ft/CMM}^2 (+)$

Orifice $H_L = 1800 \times 10^{-6} \text{ Ft/G. (X)}$

11.0

10.5

10.0

H_d

9.5

9.0

8.5

0



Orifice $H_L =$

$1575 \times 10^{-6} \text{ Ft/CMM}^2$

H.P. Carberry 6/10/80

J. F. P. 6/11/80

4000

3000

2000

1000

TIME, SECONDS

FIGURE

12

CALCULATION NO. 12846.07-PE-037-0

Sump pH values vs time after LOCA

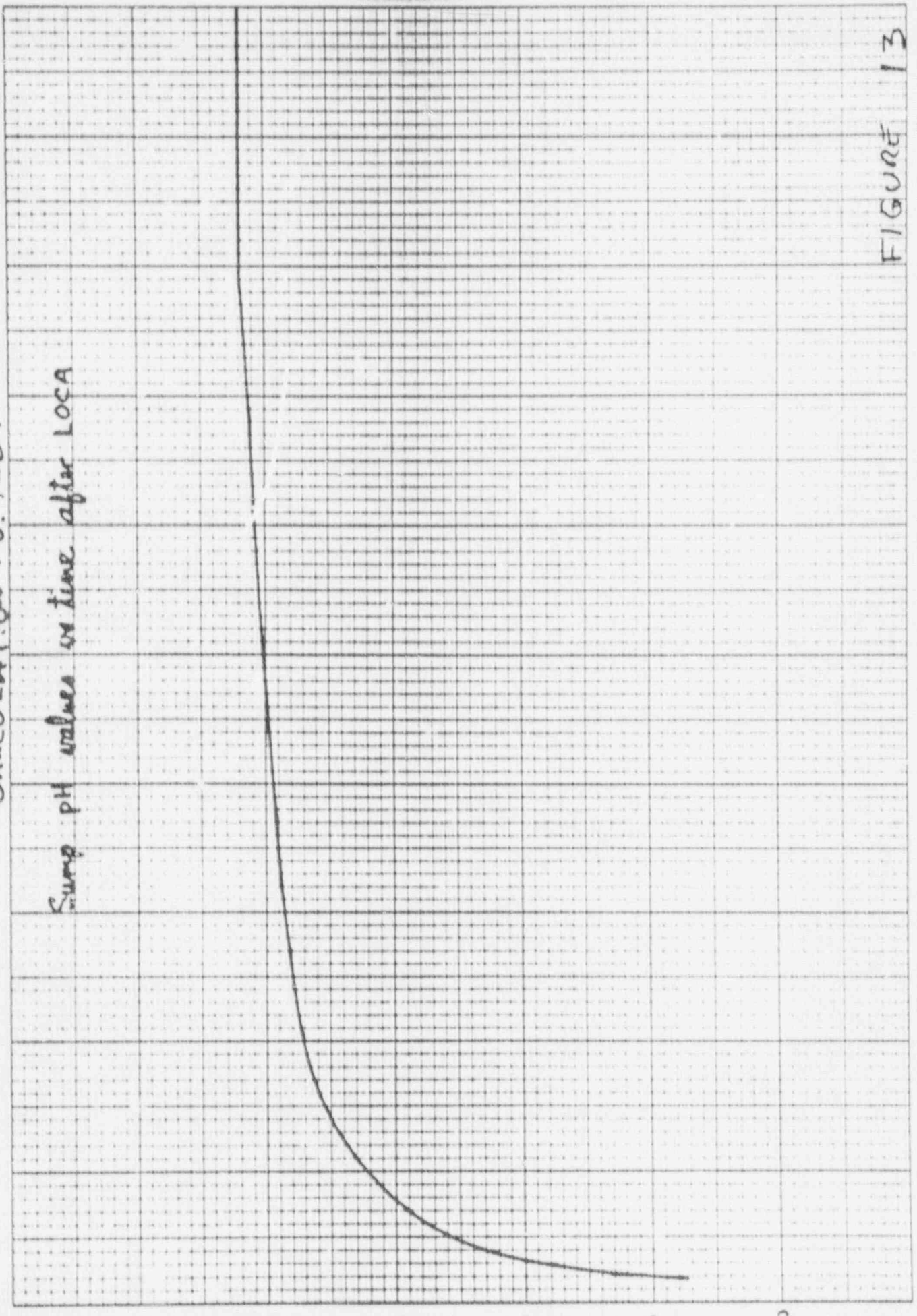


FIGURE 13

Time, Sec

PART B

CONTAINMENT SPRAY SYSTEM - SURRY #2 CAUSTIC FLUID

FLOW RATE HISTORY (CFFRH) AND CHEMICAL ADDITION

TANK (CAT.) DRAWDOWN FOR DESIGN BASIS ACCIDENT SCENARIOS

Part B contains excerpts from Stone & Webster calculation No. 12846.07/35
"Caustic Fluid Flow Rate Histories in the Containment Spray System (Containment Spray pH Analysis"):

Calc. No. 12846.07/35 Page 4 of 26	Objective of Calculation---	Page 1
Calc. No. 12846.07/35 Page 10 of 26	CFFRH Requirements	---Page 2
Calc. No. 12846.07/35 Page 12 of 26	System Schematic	---Page 3
Calc. No. 12846.07/35 Page 17 & 18 of 26	Set of Equations	---Page 4-5
Calc. No. 12846.07/35 Page 21-26 of 26	Conclusions	---Page 6-11
Calc. No. 12846.07/35 - Attach 5:	Graphical representation	---Page 12-36
	of the caustic fluid flow	
	rate history and chemical	
	addition tank drawdown.	

CALCULATION SHEET

J.O./W.O./CALCULATION NO. 12846.07 / 85	REVISION 0	PAGE 4/25
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Objective of Calculation:

To determine the Caustic Fluid Flow Rate History (CFRTH) in the Containment Spray System for a caustic solution concentration of $17.5\% \pm 0.5\%$, under the following modes of operation and assumptions (accident scenarios):

SCENARIO No	PUMPS IN OPERATION			ASSUMPTION		
	CS	LH	HH	MAX SPRAY pH	MIN SPRAY pH	MIN SUMP pH
1	1	1	1	✓		
2	2	2	2	✓		
3	1	2	2	✓		
4	2	1	1	✓		
5	1	1	1		✓	
6	2	2	2		✓	
7	1	2	2		✓	
8	2	1	1		✓	
9	1	1	1			✓
10	2	2	2			✓
11	1	2	2			✓
12	2	1	1			✓

- CS = Containment Spray Pump(s)
- LH = Low Head Safety Injection Pump(s)
- HH = High Head Safety Injection Pump(s)

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4 - CFRRH requirements:

a) At any time during caustic injection:

$$\text{Min Allowable Flow Rate} < \text{Predicted Flow Rate} < \text{Max. Allowable Flow Rate}$$

(Flow Rate corresp. to pH=8.5) (Flow Rate corresp. to pH=11.0)

b) CAT gets empty before RWST gets empty.

Note: Max and Min Allowable Flow Rates are determined in Attachment No 1.

5 - Determine CFRRH for all accident scenarios specified on page 4, with no restrictive orifices, to demonstrate whether or not direct suction flow from the CAT is feasible and whether or not restrictive orifices are required.

Direct suction flow is not feasible if during caustic injection:

$$\text{Predicted Flow Rate} < \text{Min. Allowable Flow Rate}$$

Restrictive orifices are required if:

$$\text{Predicted Flow Rate without orifices} > \text{Max Allowable Flow Rate}$$

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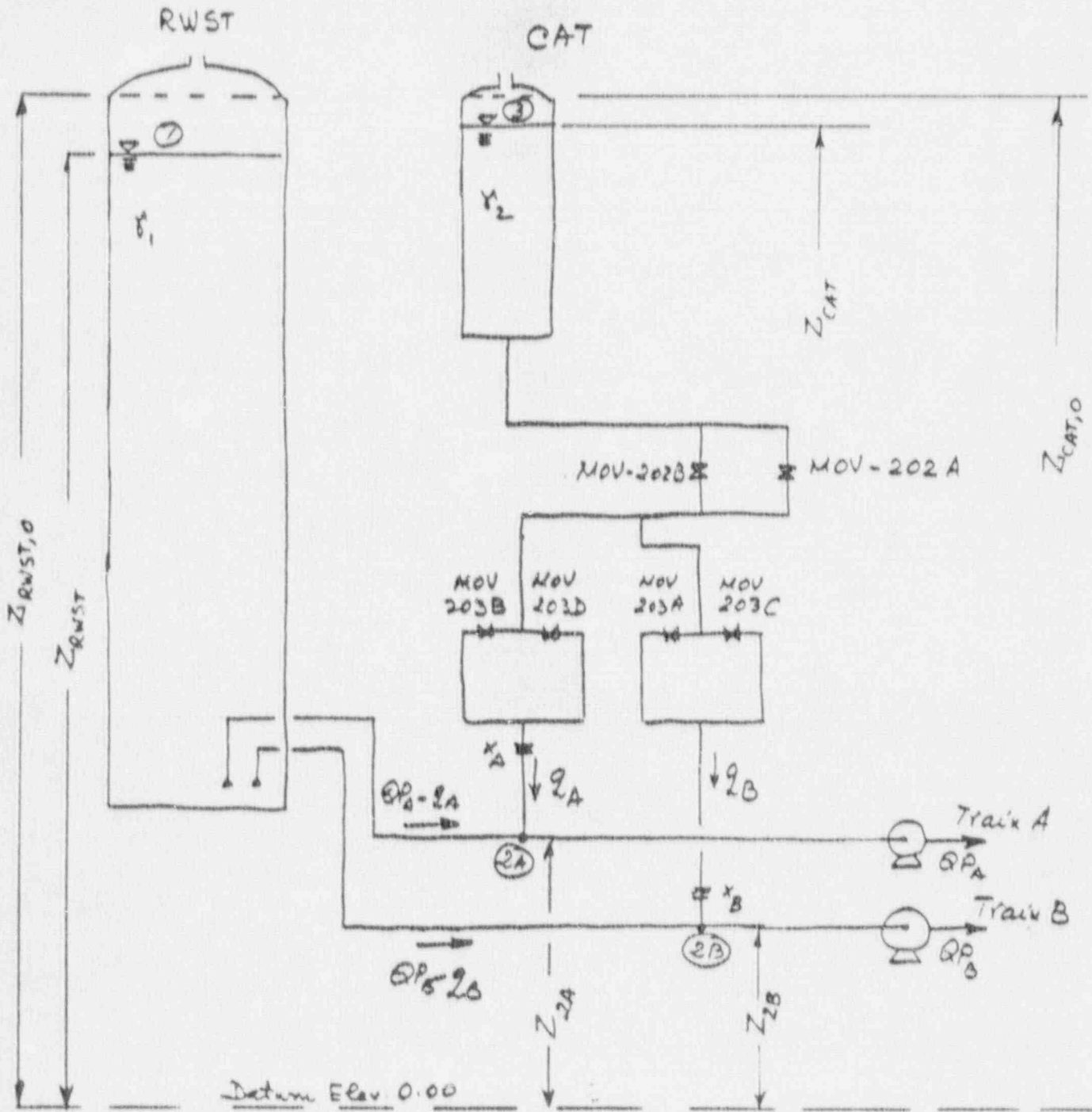
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Direct Suction System Schematic



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C = F R H in the Containment Quay System

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The set of equations is:

$$Z_{CAT}(0) \rightarrow \text{known}$$

$$q_{2A}(l) = \frac{1}{\sqrt{K_{3-2A} + X_A}} \sqrt{Z_{CAT}(l) - Z_{2A} - \frac{S_{RWST}}{S_{CAT}} + E_{2A}(l)} \quad (1)$$

$$q_{2B}(l) = \frac{1}{\sqrt{K_{3-2B} + X_B}} \sqrt{Z_{CAT}(l) - Z_{2B} - \frac{S_{RWST}}{S_{CAT}} + E_{2B}(l)} \quad (2)$$

$$Z_{CAT}(l+1) = Z_{CAT}(l) - 0.0085233 * \left[\frac{q_{2A}(l)}{K_A} + \frac{q_{2B}(l)}{K_B} \right] * \Delta t_{min} \quad (3)$$

Notes:

- K_{3-2A}, K_{3-2B} are constant parameters (head loss coef between the CAT and the Junction Points $2A, 2B$ without the restrictive orifices - Ft/GPM²); the numerical values of K_{3-2A}, K_{3-2B} are specified on pages 6 and 8.
- X_A, X_B are constant parameters (head loss coef through the restrictive orifices); numerical values of X_A, X_B are selected as described on page 11.
- Z_{2A}, Z_{2B} constant numerical values (see page 16) in Ft.

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CFRTH in the Containment Spray System

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- S_{RWST} , S_{CAT} are constant parameters (sp. gr. of the Boric Acid solution and caustic solution); numerical values as specified on pages 6 and 8.
- $Z_{CAT}(0)$ is a constant parameter (initial elevation of the caustic solution in the CAT); numerical values as specified on pages 5 and 7 in Ft.
- Δt_{min} is a constant numerical value (integration time), selected arbitrarily $\frac{1}{3}$ min, (20 sec)
- $E_{2A}(i)$, $E_{2B}(i)$ are variables (pressure and kinetic energy at the junction points in Ft. of Boric Acid solution).
 $E_{2A}(i)$ and $E_{2B}(i)$ are calculated and analytically expressed in Attachment #1

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CFRRH in the Containment Spray System.

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Conclusions:

- 1 - The "direct suction flow" method for chemical addition is feasible since without any control (orifice) the flow rates from the CAT exceed the max. allowable flow rates (See Attachment No 5, $x_A = x_B = 0$ case)
- 2 - With an orifice $x_A = x_B = 1575 \times 10^{-6}$ FT/GPM² the flow rates from the CAT can be kept between the min and the max. allowable flow rates, or the pH can be maintained between 8.5 and 11.0 for all accident scenarios analyzed. (See Attachment 5)
- 3 - With an orifice $x_A = x_B = 1575 \times 10^{-6}$ FT/GPM² the CAT will empty before the RWST, hence, under any of the accident scenarios analyzed the entire volume of caustic solution in the CAT will be pumped by the containment spray pumps into the reactor containment.

Considerations regarding the sensitivity of the calculation and input data.

- 1 - Input data: The calculated flow rates and CAT drawdown for each accident scenario represent max or min envelopes rather than the actual flow rates or drawdown which can be expected. All the inputs were analyzed and then selected.

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In such a way to form two sets of consistent inputs, one to maximize the flow rates (pH), the other one to minimize the flow rates (pH). The inputs considered parametric in the calculation are as follows:

- The RWST initial elevation, including the instrument error
- The CAT initial elevation, including the instrument error
- Caustic solution concentration
- Caustic solution temperature
- Boric Acid solution concentration

The fact that in developing the max or min envelopes, ^{all} the parametric values were selected either to minimize or to maximize the results, is a guaranty that sufficient conservatism does exist in the results of the calculation.

2- Calculations

There are two parameters, namely the head loss coefficient between the RWST and the Junction Point, and the head loss coefficient between the CAT and the Junction Point which are essential in estimating the CAT flow rates and draw down. These two coefficients were

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analytically calculated and then verified by way of a field test (RWST-CAT Drawdown Test 4/30/80 - See Ref. 6). The results of the field test showed that the actual head losses were 2.6% greater than their analytical evaluation. In order to simplify the sensitivity analysis of the head losses, the calculation was performed with head loss coefficients between RWST and Junction Point modified, to include a margin of uncertainty of $\pm 5\%$, while the CAT-Junction head loss coefficient was kept at its calculated value. However, a sensitivity analysis of the head loss between the CAT and Junction Point shows that while the design orifice head loss coefficient is $1575 \times 10^{-6} \text{ Ft/GPM}^2$, the CFRH requirements are met for any coefficient between $1350 \times 10^{-6} \text{ Ft/GPM}^2$ and $1800 \times 10^{-6} \text{ Ft/GPM}^2$. The head loss coefficient of the CAT piping system without the restrictive orifice was considered parametric, between a min of $420 \times 10^{-6} \text{ Ft/GPM}^2$ and a max of 520 Ft/GPM^2 (See pages 6 and 8). The total head loss coefficients between the CAT and Junction Point for which the CFRH requirements are met

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are as follows:

$$\text{Max: } K = 1800 \times 10^{-6} + 520 \times 10^{-6} = 2320 \times 10^{-6} \text{ Ft/GPM}^2$$

$$\text{Design: } K = 1575 \times 10^{-6} + 470 \times 10^{-6} = 2045 \times 10^{-6} \text{ Ft/GPM}^2$$

$$\text{Min: } K = 1350 \times 10^{-6} + 420 \times 10^{-6} = 1770 \times 10^{-6} \text{ Ft/GPM}^2$$

The above coefficients show that the head losses between the CAT and Junction Points could vary $\pm 13\%$ without affecting the CFRRH requirements.

3 - Predicted CFRRH and CAT Drawdown

The calculated caustic flow rates and CAT drawdown are based on the set of equations shown on page 17. The set of equations models the hydraulics of the RWST and CAT drawdowns as a succession of steady state conditions since certain hydraulic parameters change gradually with time. In order to demonstrate that this analytical approach can rigorously model the CAT drawdown, a field test was performed on 4/30/80. The results of this test (see Ref 6) show that from a practical stand point there are no differences between measured and calculated values and therefore the analytical method can accurately model the CAT drawdown. However, the margin of uncertainty is

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of the CAT drawdown measurements was approximately ± 4 inches (Ref 6) and therefore the same margin of uncertainty can be attributed to the calculated drawdown.

Assuming that a difference between calculated and actual CAT drawdown could exist, a legitimate concern could be derived regarding the capability of the drawdown to empty the CAT before CS pump(s) shutdown. In order to analyze the criticality of this concern, scenario W-11 was selected for testing the sensitivity of the CAT drawdown possible margin of uncertainty. (Scenario W-11 is the most critical case regarding the CAT drawdown). Under design conditions (orifice head loss coef 1575×10^{-6} Ft/GPM²) the CAT is almost empty at 3860 sec. after the start of the accident (CAT Elev. 34.1 Ft), approximately 115 sec. before the shutdown of the CS pump which occurs at time 3975 sec. If at 3860 sec. the CAT is not empty, there are approximately 2 min available to eventually empty the CAT. The drawdown corresponding to an orifice of 1800×10^{-6} Ft/GPM² head loss coefficient shows that at 3860 sec. the CAT elev. is 34.9 Ft, or approximately 9.6 inches above CAT elev. of 34.1 Ft and the CAT is empty at

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approximately 3980 sec.

This demonstrates that even with a margin of uncertainty of 9.6 inches the CAT drawdown will not be critical, the CAT will empty before CS pump shut down, and the spray pH will be between the two 8.5 and 11.0 limits.

CALCULATION SHEET

STONE & WEBSTER ENGINEERING CORPORATION

Attn: Mr. T

J.O./W.O./CALCULATION NO. 12846.07 / 35		REVISION 0	PAGE 1/25
PREPARED / DATE Oscar Faires 6/5/80	REVIEWER / CHECKER / DATE P. O'NEIL 5 JUNE 80	INDEPENDENT REVIEWER / DATE Alan Sam 6/10/80	
SUBJECT / TITLE CFFRH in the Containment Stay System		QA CATEGORY / CODE CLASS I	

Graphical Representation of the Caustic Fluid Flow Rate History (CFFRH) and CAT Drawdown:

1 - CFRRH - pages 2 - 13

Legend:

- 2CAT — Max and Min flow rates corresponding to pH of 11.0 and 8.5
- △—△—△ Flow Rate Time History without restriction on flow
- Design Flow Rate History
- } Flow Rate Time History for sensitivity analysis
- } (assuming ± 13% fluid loss maximum in the caustic lines and restriction on flow)

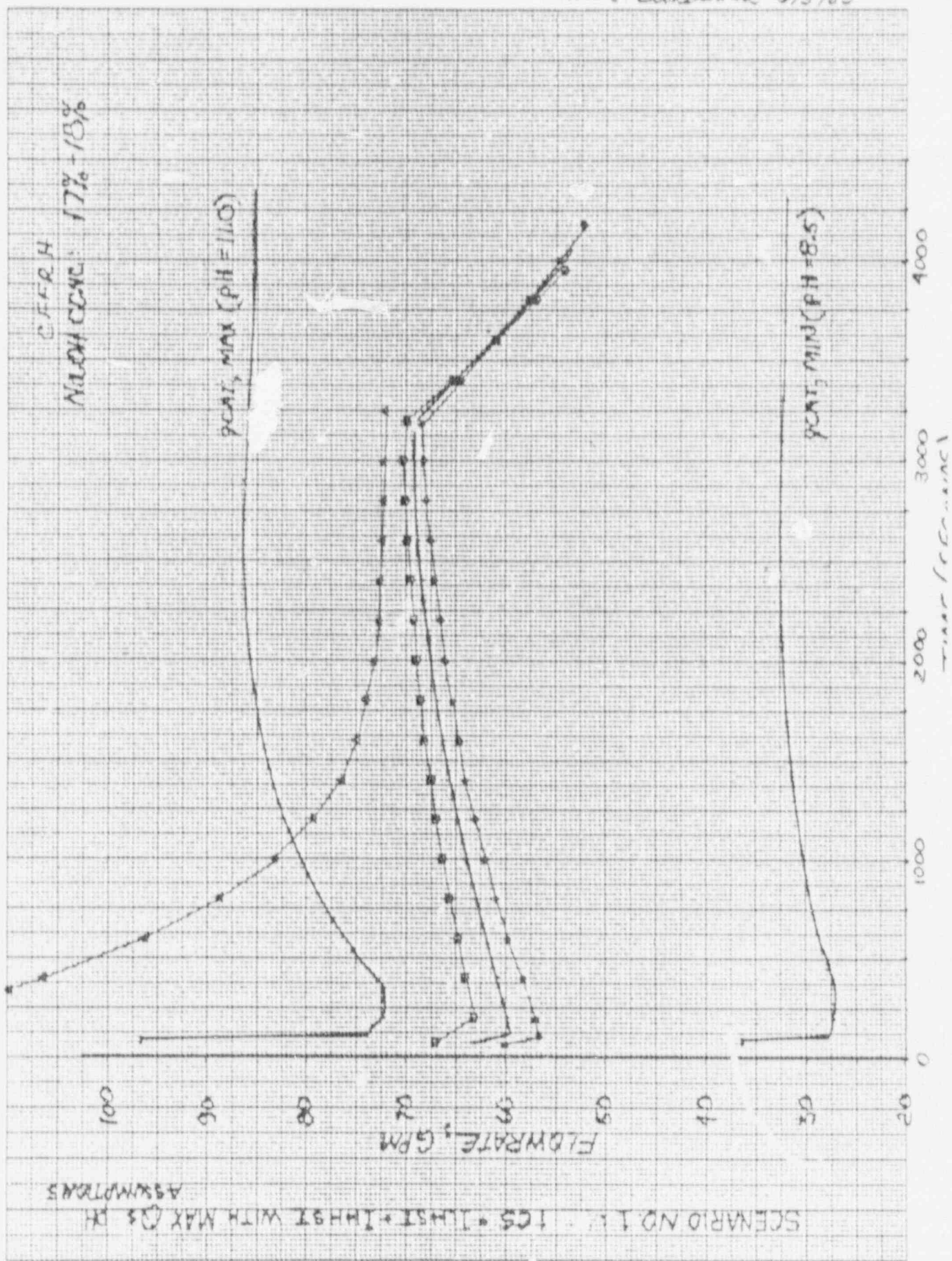
2 - CAT Drawdown - pages 14 - 25

Legend:

- Design Drawdown

461510

K-E 10 A 10 TO THE CENTIMETER 8 x 10 CM
MAGNIFY 8500 X CO. MADE IN U.S.A.



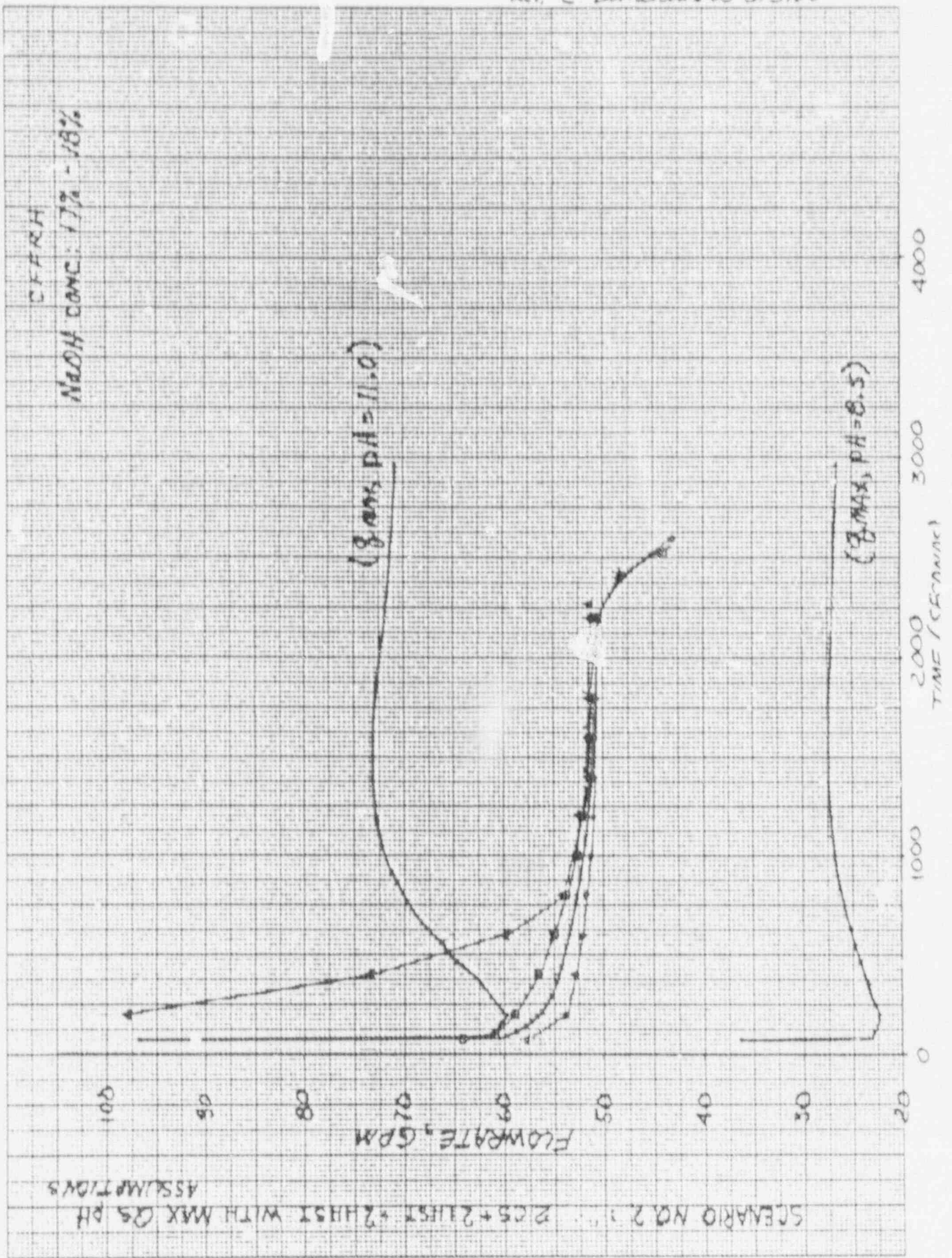
Calc No 12846.07/35

ATTACHMENT NR 5

P9 3/25

PREP: P. ONBIL 23JUN80

REV: C. THOMPSON 3/5/80



461510

K-E 10 X 10 TO THE CENTIMETER

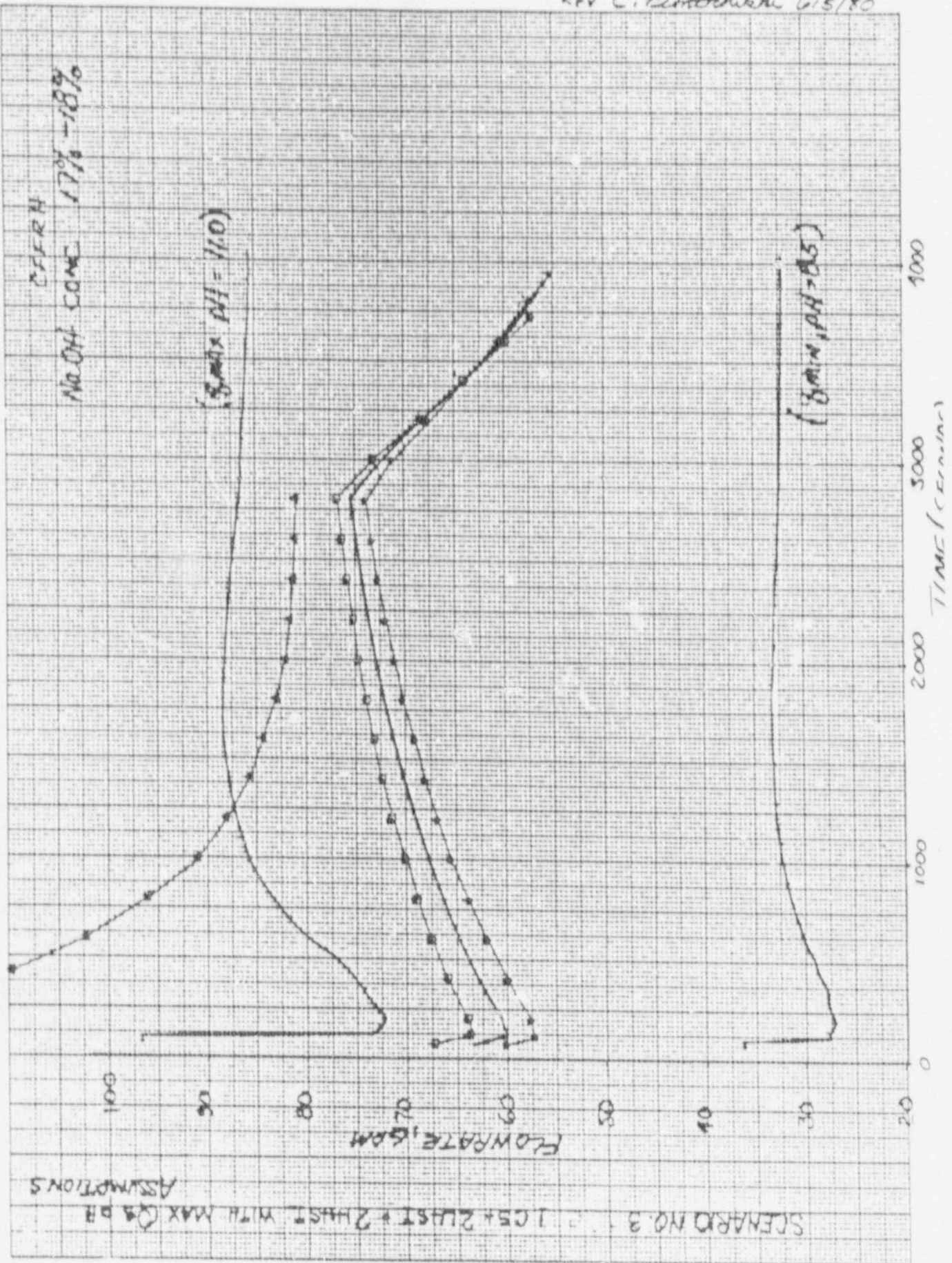
Calc. No 12646.07/35

ATTACHMENT NR 5

pg. 4/25

PREP: P. O'NEIL 2/19/80

REV C. LINTON 4/15/80

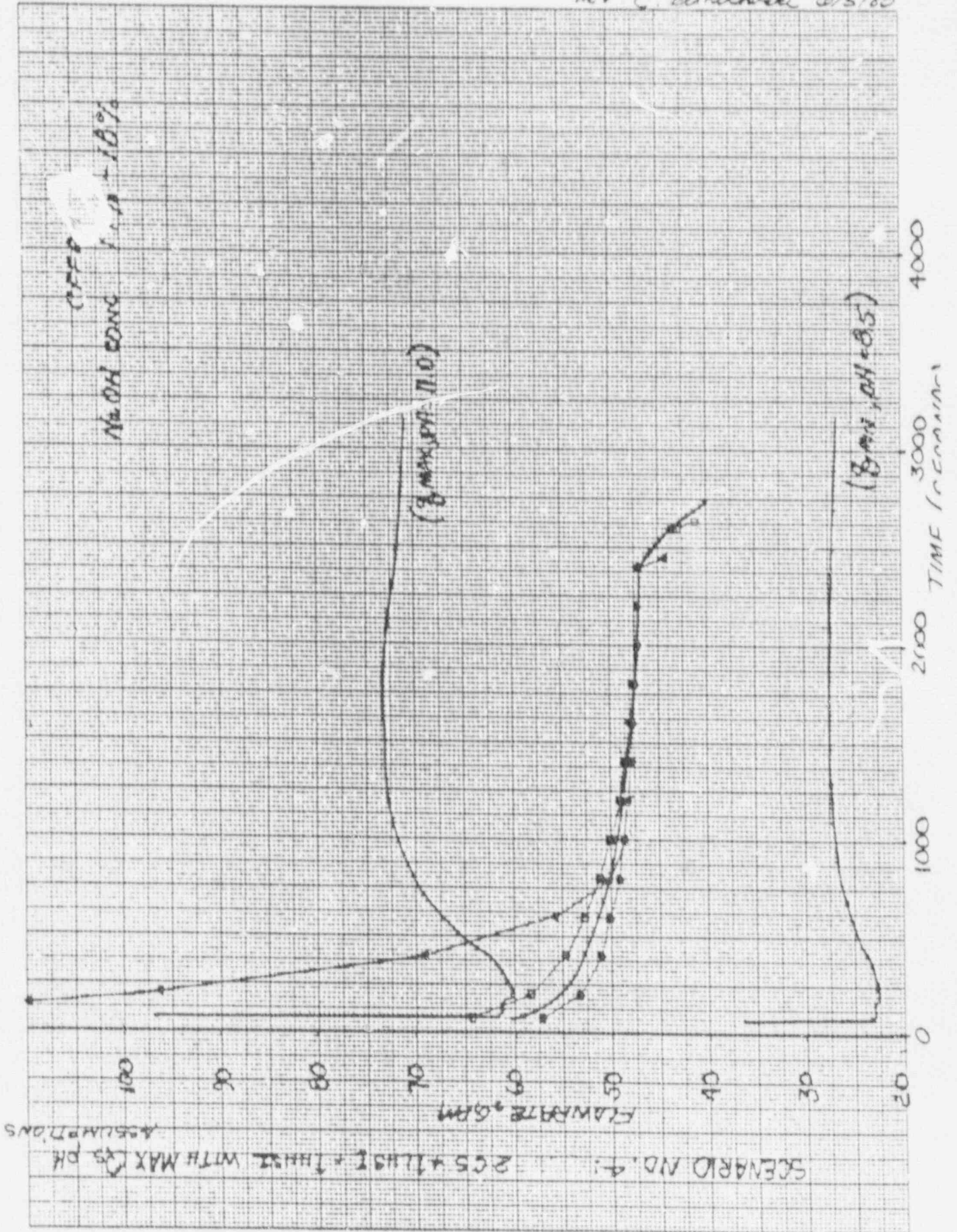


Calc. No 12846.07/35

ATTACHMENT N 5 pg 5/25
PREP: P. ONEIL 2/21/80
REV: C. [unclear] 6/5/80

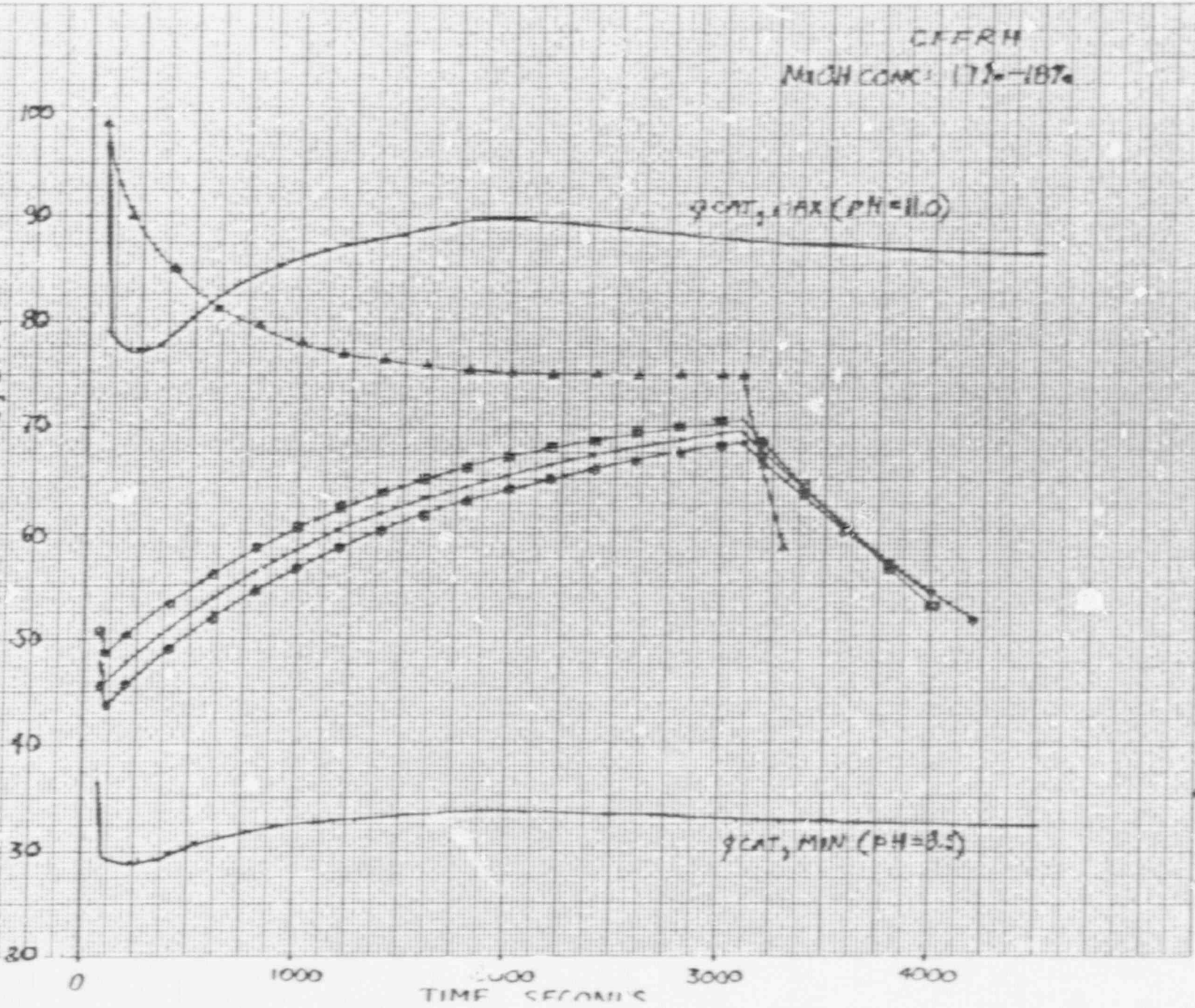
461510

K-E 12 X 10 TO THE CENTIMETER 4 X 10 M
MILWAUKEE & SONS CO.



SCENARIO NO. 5, 1CS + 1GHSJ + 1HHSJ WITH MIN Q₅
pH ASSUMPTIONS

FLOWRATE, GPM

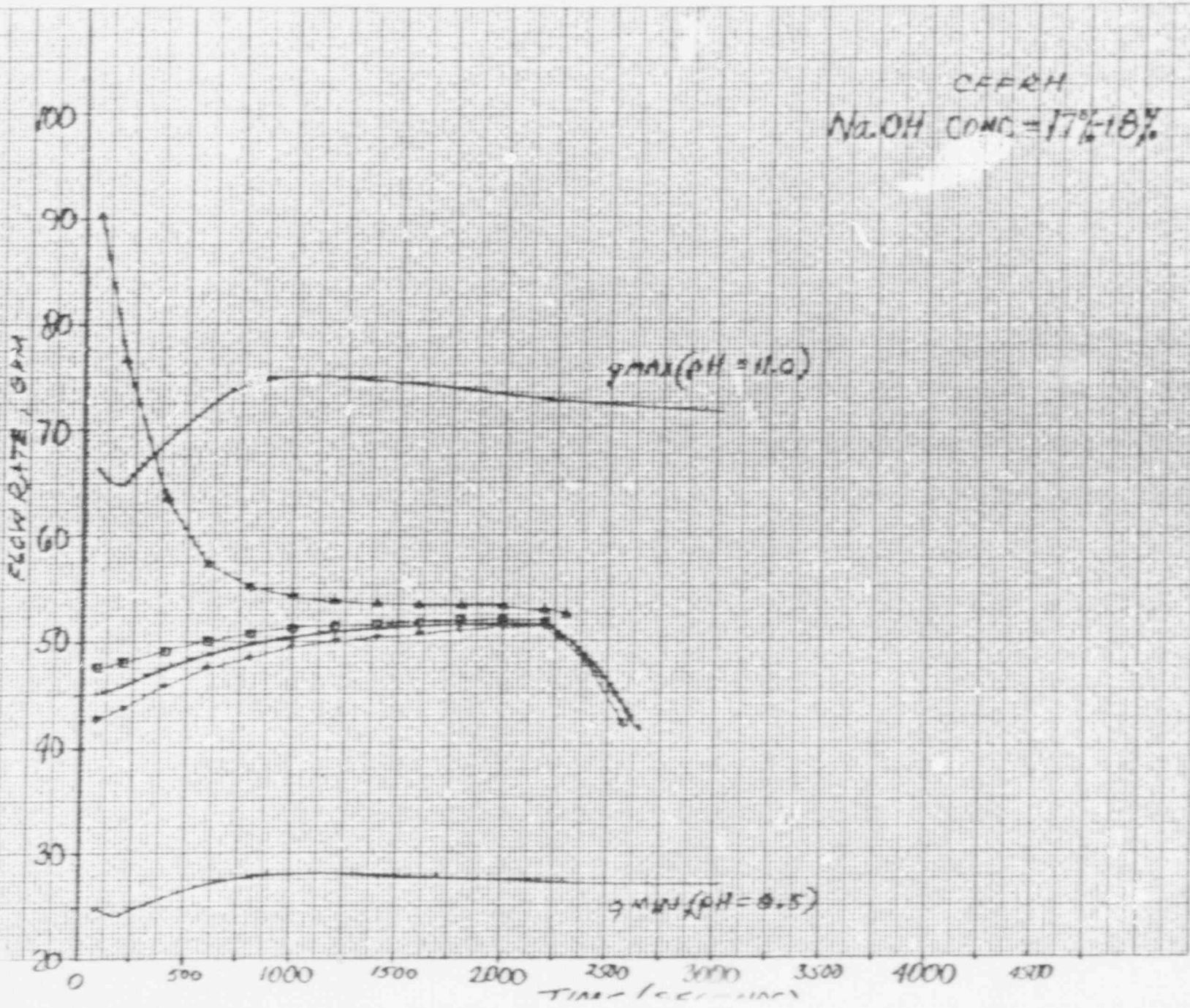


CFRHM
MICH CONC: 17% - 18%

Calc. No 1204607/3r ATTACHMENT NO 5
P. 0201 SOURCE P. 6/25
REV. C. SANDERSON 01/5/80

12

SCENARIO NO. 60: 2CS + 2LHST + 2HST WITH MIN QS
PH ASSUMPTIONS



Calc. #1 12846.07/35
ATTACHMENT NR 5 PG. 7/25
PREP. P. ONEL 3 JUNE 80
REV. C. FERRERON 6/15/80

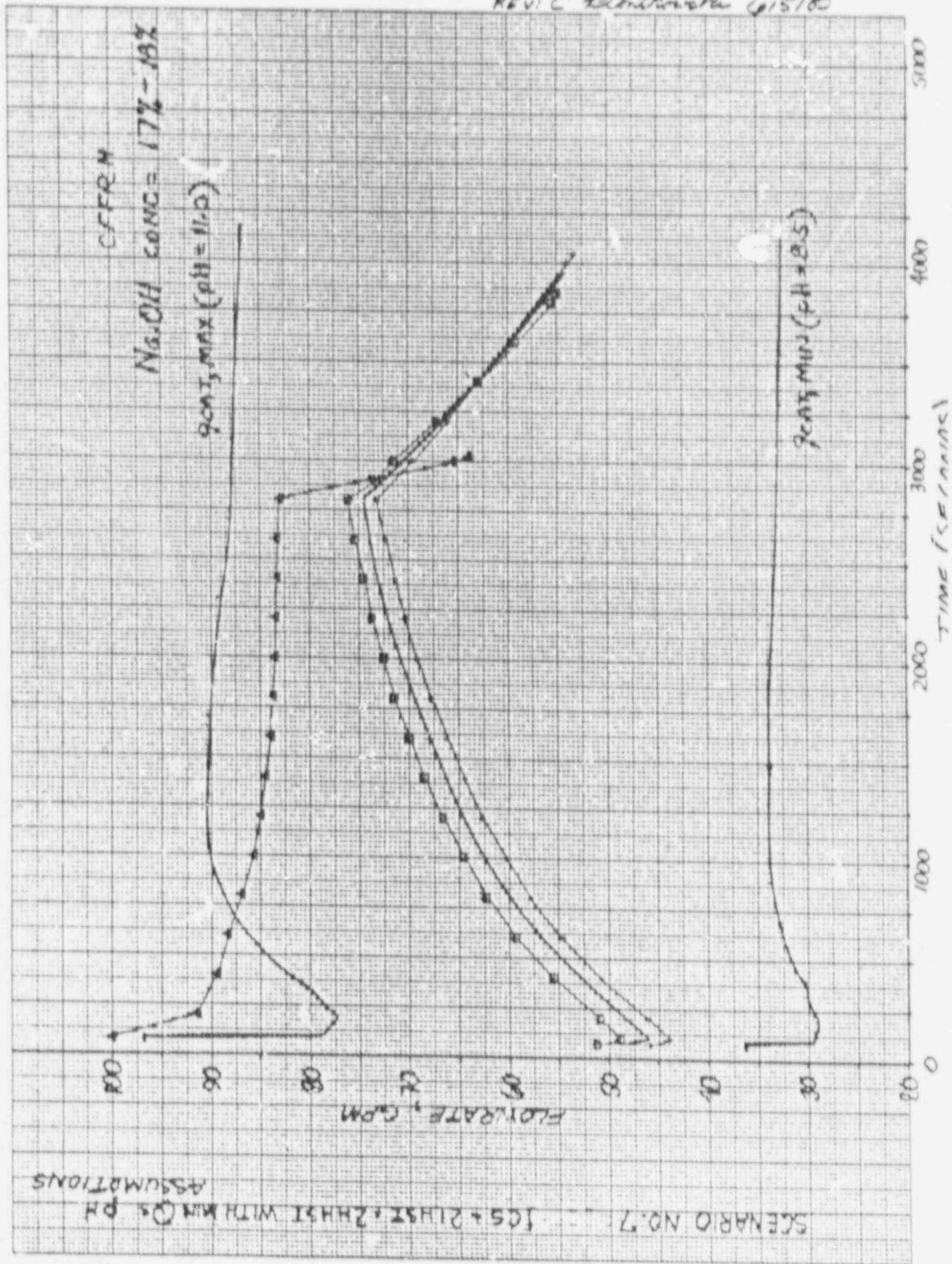
18

Case No 12846.07/35

ATTACHMENT NO 5
PREP: P. O'NEIL 3/31/80
REV: C. [unclear] 4/15/80

461510

K-E 10 X 10 TO THE CENTIMETER 4 X 2 CM
HUPFEL & BAKER CO. MADE IN U.S.A.



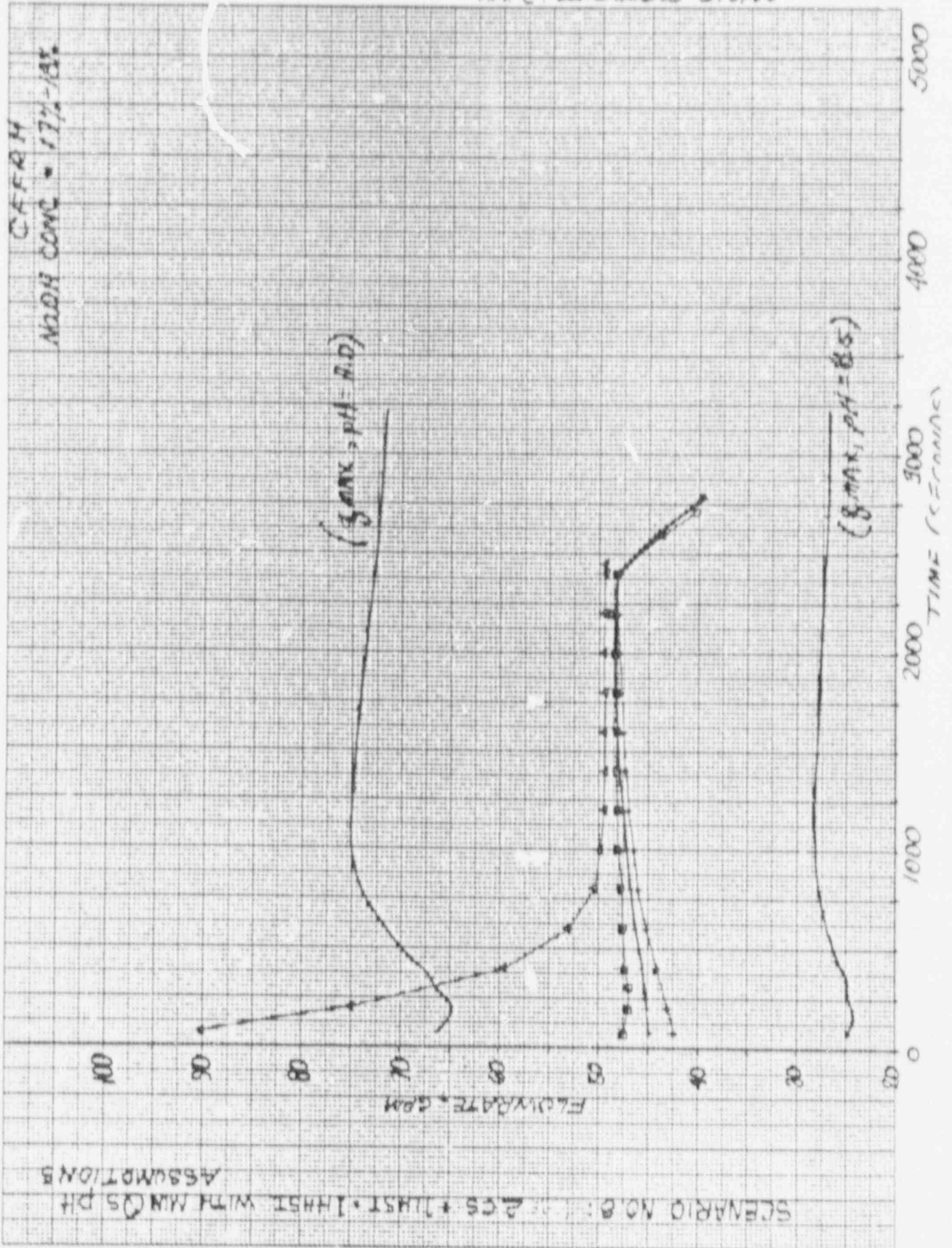
Calc # 254507/35

ATTACHMENT NO. 5
PREP. P. O'NEIL 3/28/80
REV. C. BENTON 6/15/80

pg. 9/25

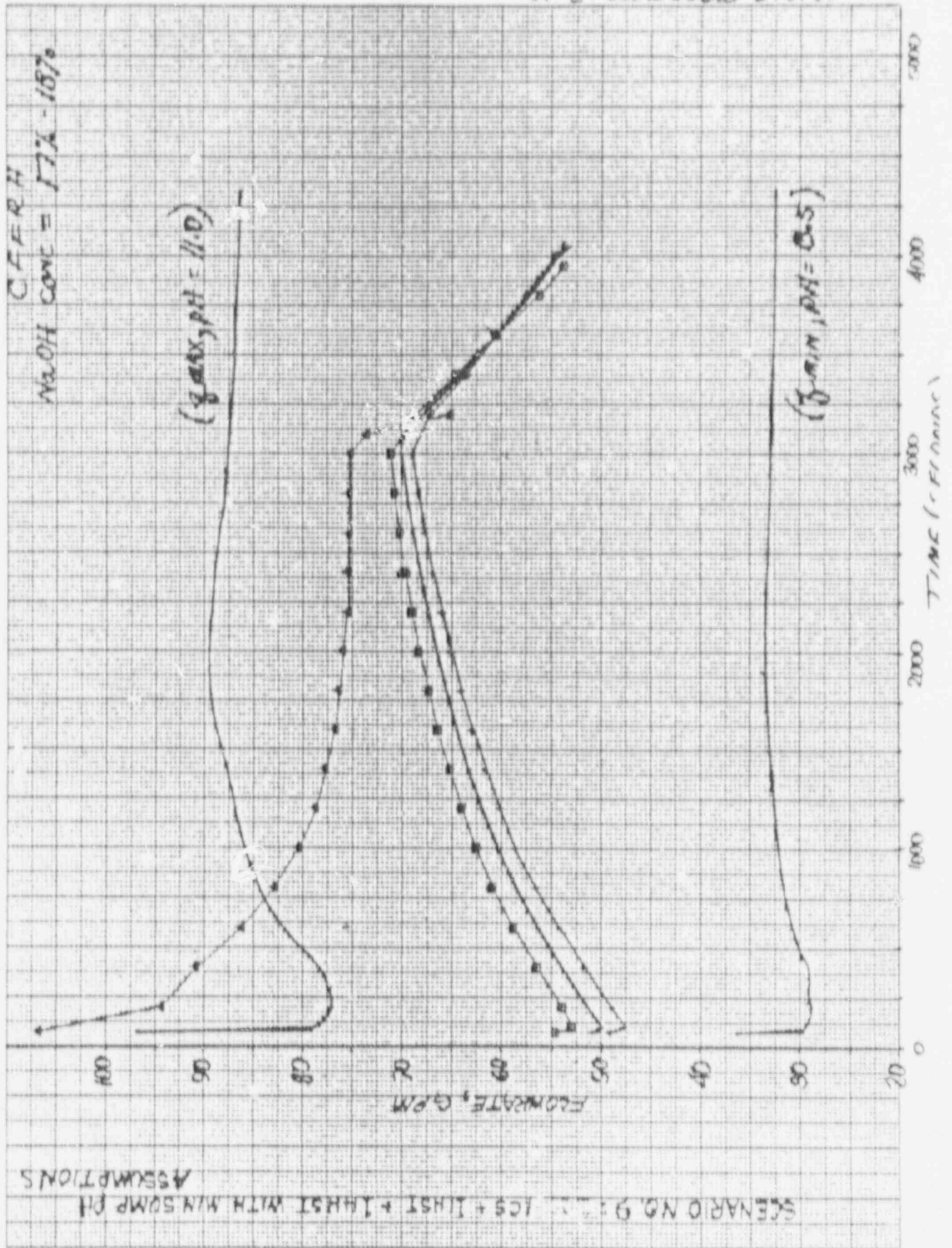
461510

K-E 15 x 10 TO THE CENTIMETER
WEIGHT & EDGE CO.



Case No 12846.07/35

ATTACHMENT NO 5 P3. 10/25
PREP: P. O'NEIL 3/24/80
REV: C. [unclear] 6/5/80

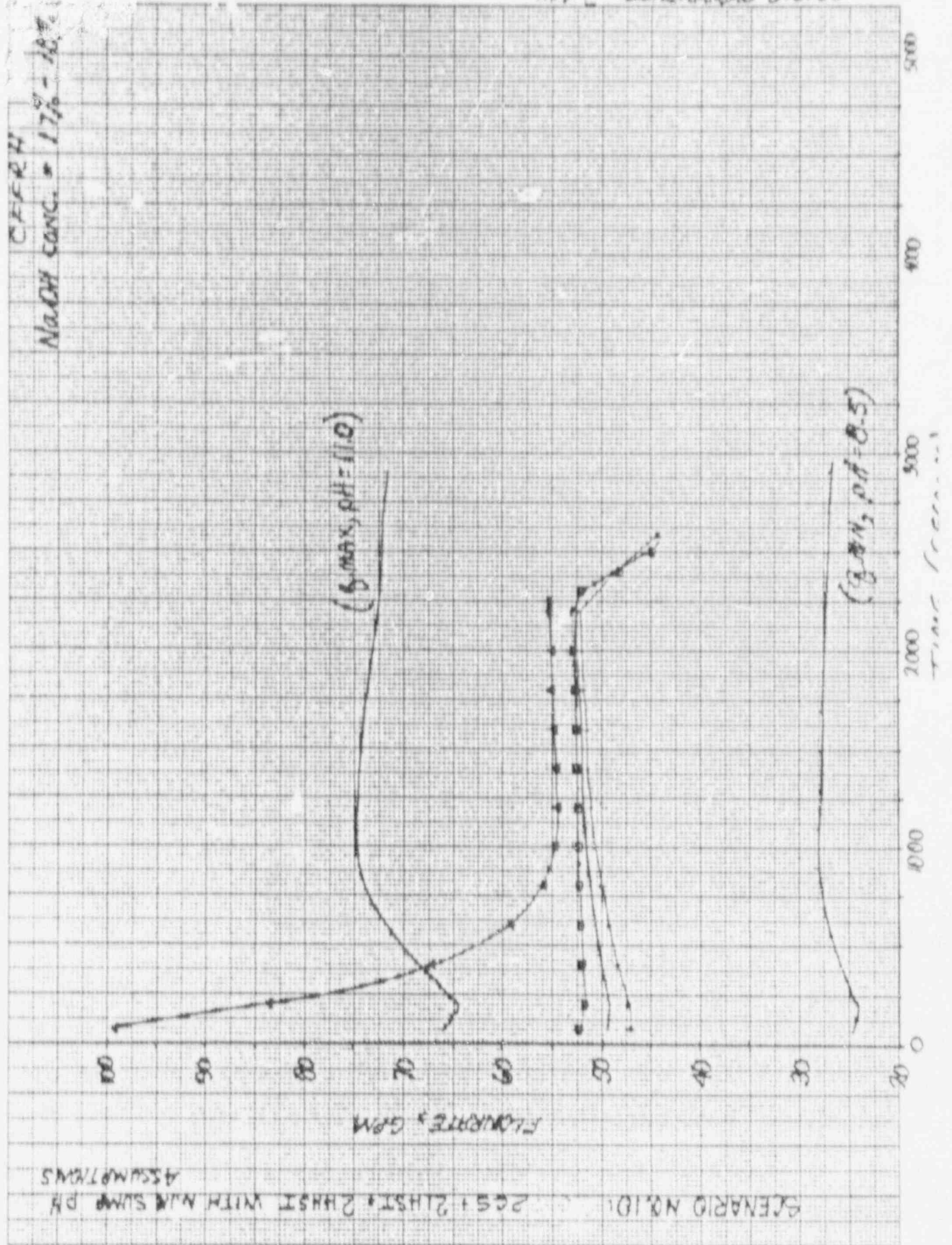


451510

K-E 10.0 TO THE CENTIMETER
REPAIRED & RECALIBRATED

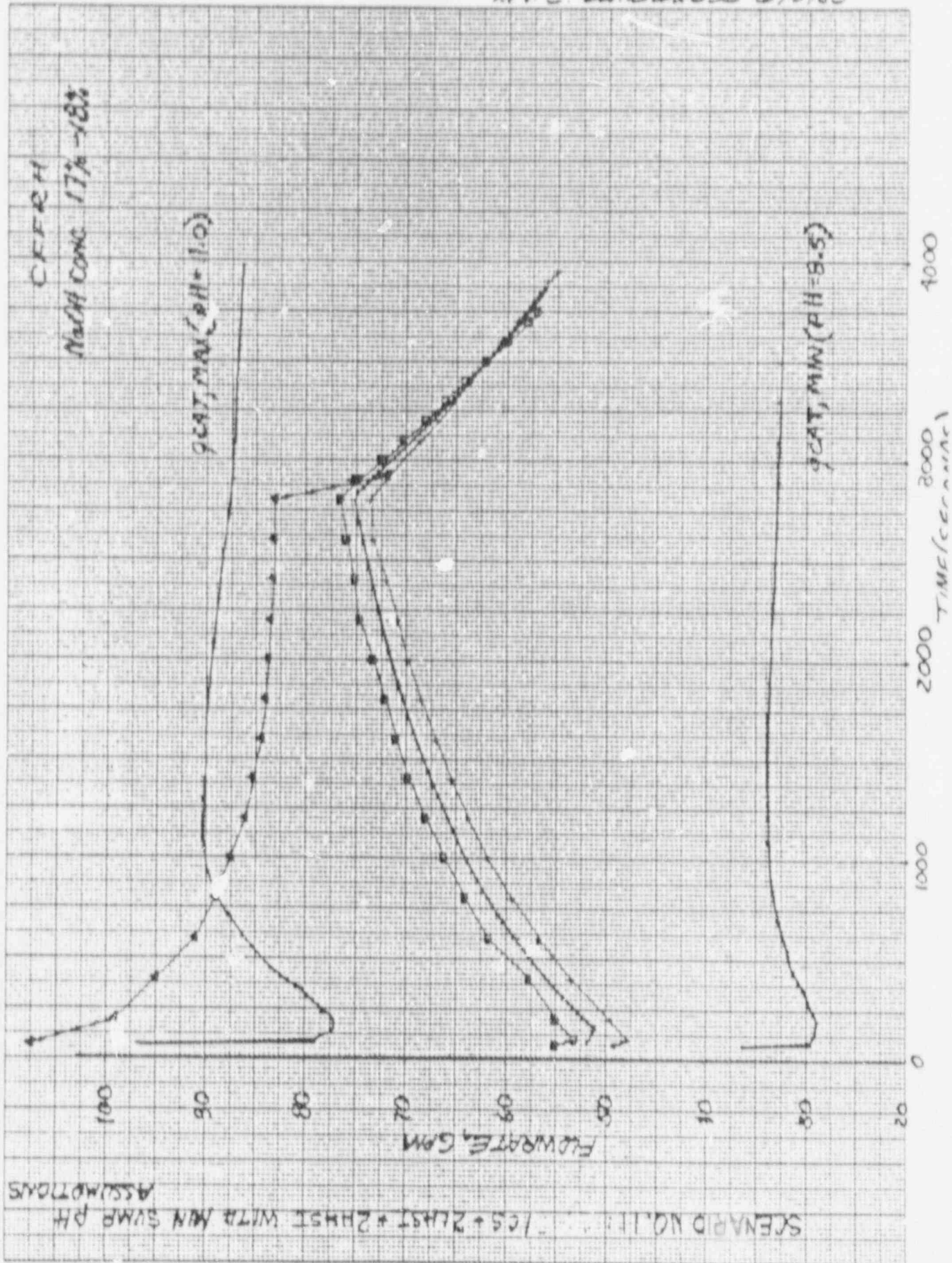
Case # 12846.07/95

ATTACHMENT NO 5
PREP: P. ONEIL SJINER PG. 11/25
REV: C 01/5/80



461510

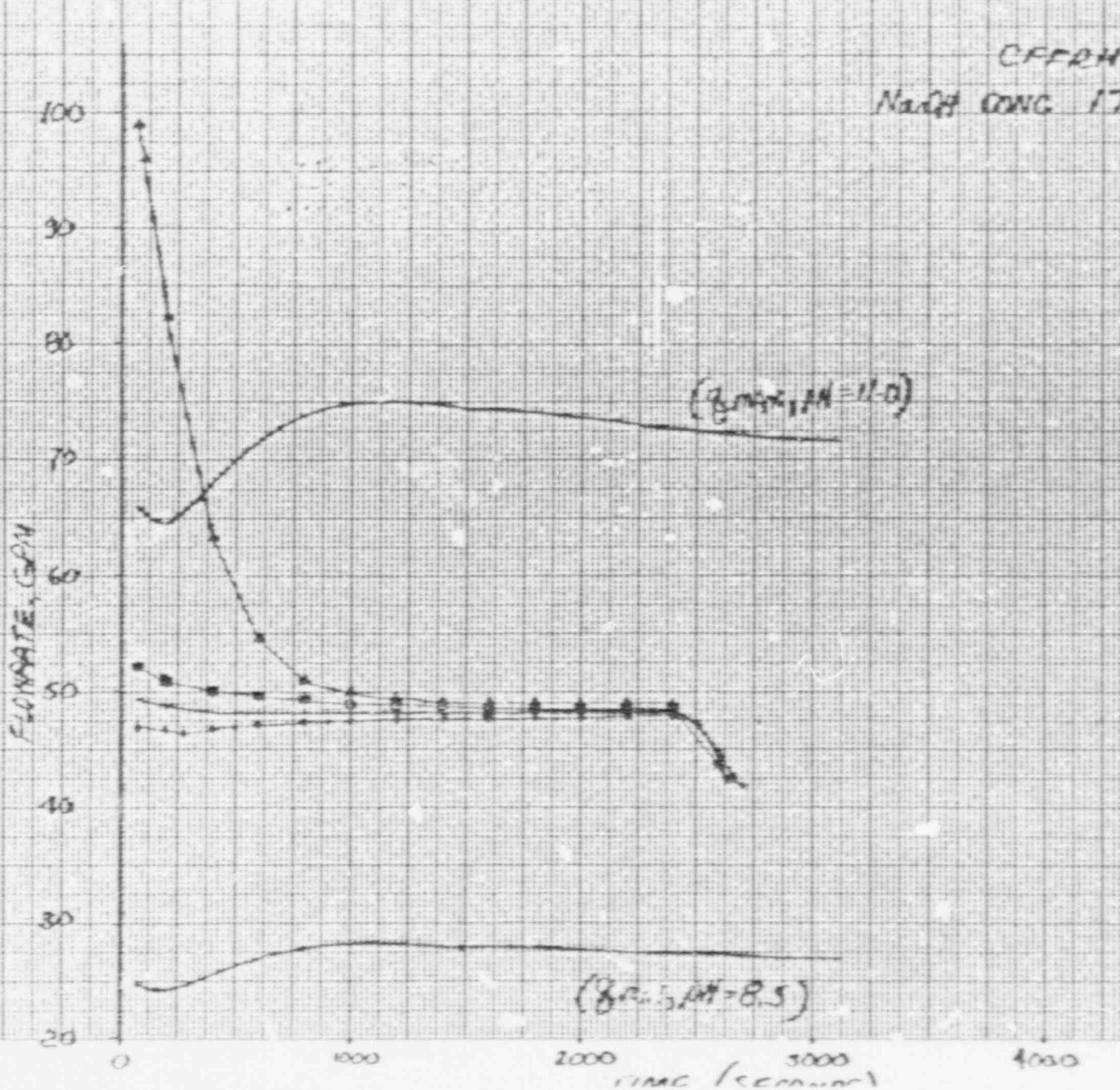
H-E 10 x 10 TO THE CENTIMETER 4 x 4 INCH
SPECIAL & REGULAR CO. MADE IN U.S.A.



461510

K-E 15 X 15 TO THE CENTIMETER 18 X 25 CM
 HOPKIN & BOWEN CO. MADE IN U.S.A.

SCENARIO NO. 12: 2GB + 1LHST + 1LHST WITH MAX SWMP
PH ASSUMPTIONS



Calc No 12846.07/3r

ATTACHMENT NO 5
PREP: P. ONEL 5046 00 P. 12/25
REV: C Rindenburg 01/5/82

12

DRAWN BY: J. O'NEAL
CHECKED BY: J. O'NEAL

SCENARIO 1b.1 : 1CS + 1LH + 1HH WITH MAX. STAY P-I.A. ASSUMPTIONS

CALC. 12086607/35

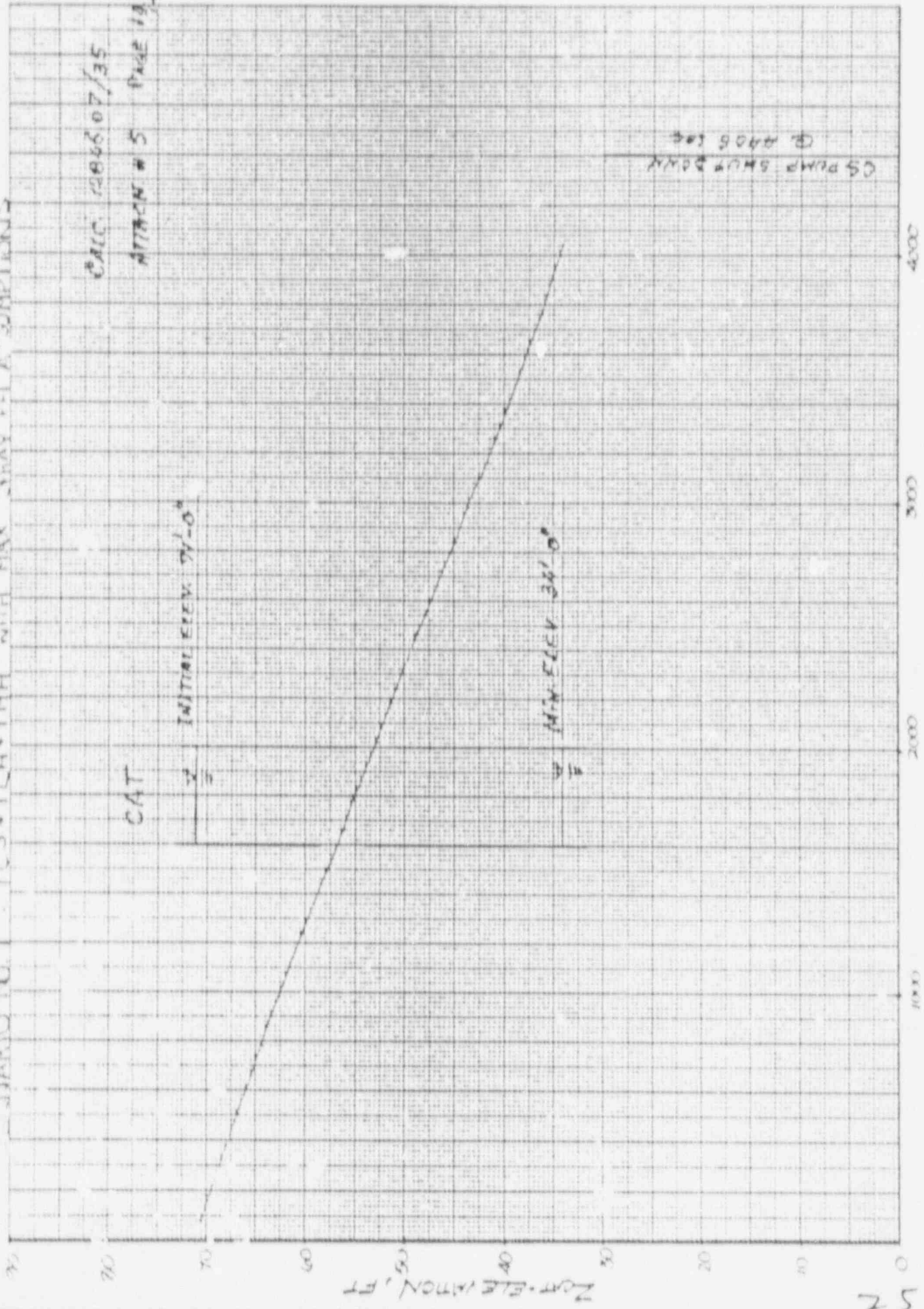
ATTACH # 5 PAGE 19/25

CAT

INITIAL ELEV. 24'0"

MIN. ELEV. 34'0"

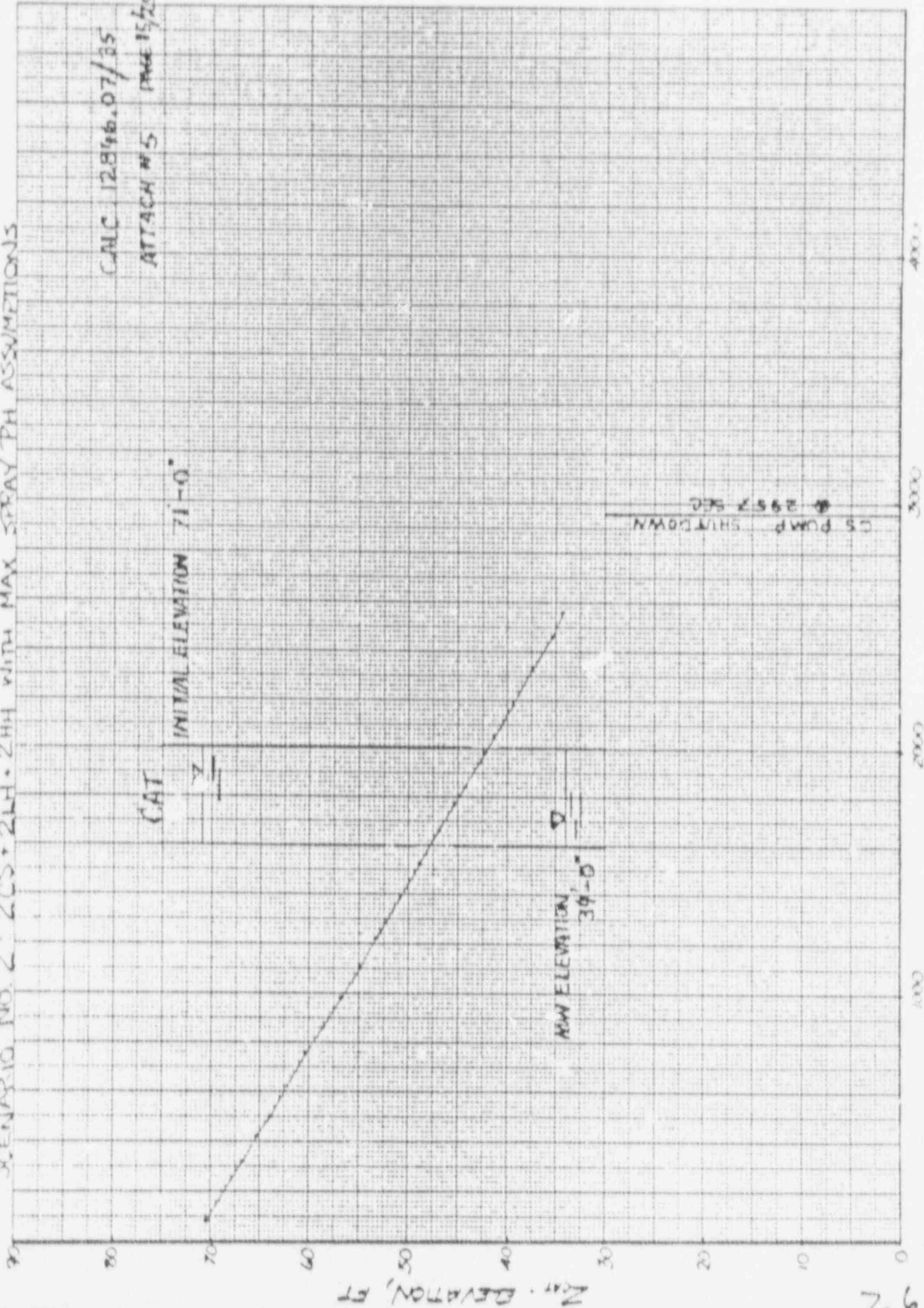
CS PUMP SHUT DOWN @ 2408 LAG



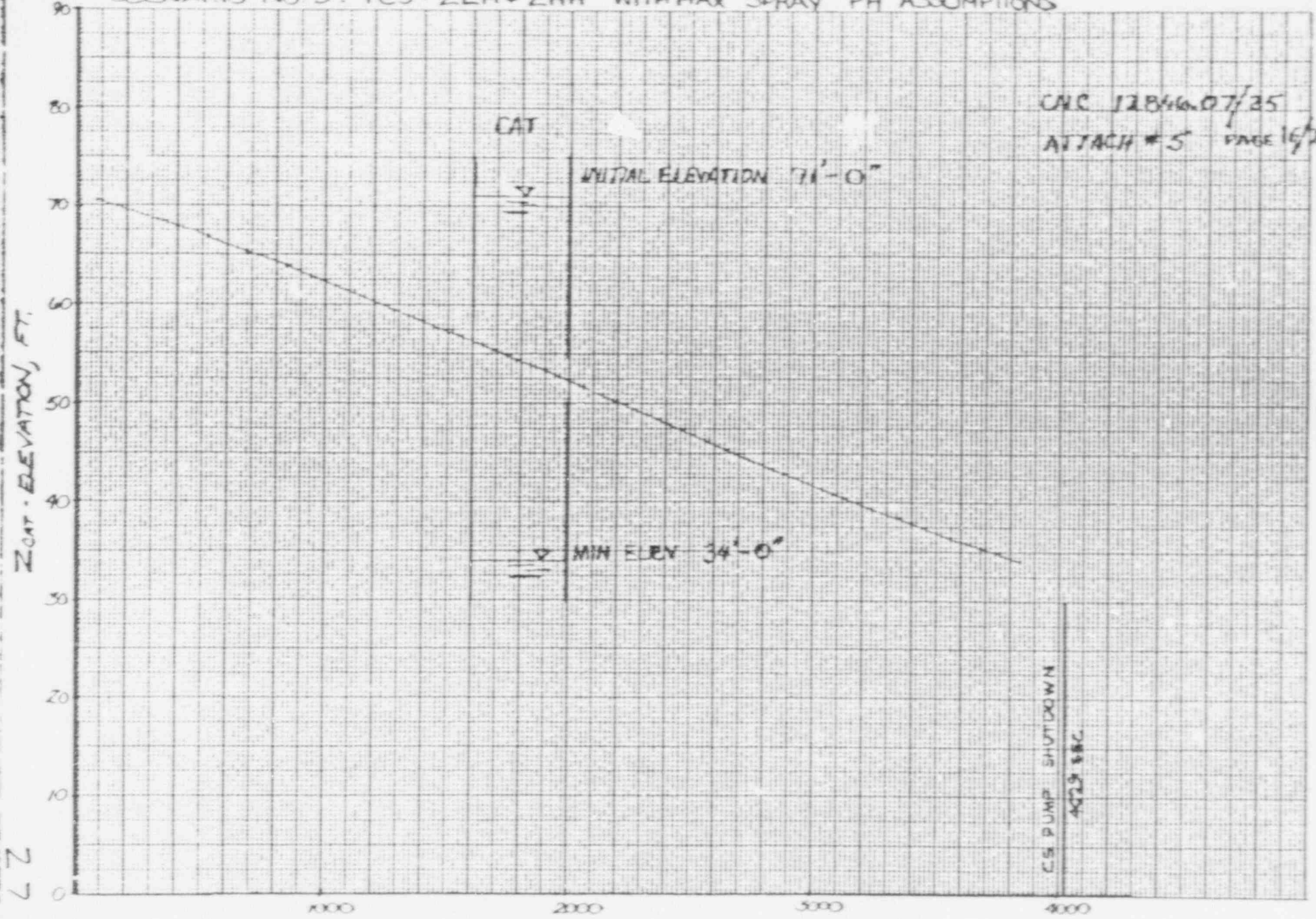
PREPARED: C. THOMPSON 6/3/80
CHECKER: P. O'NEIL 5 JUNE 80

SCENARIO No. 2: 2CS + 2LH + 2HH WITH MAX SPRAY PH ASSUMPTIONS

CALC 128/66.07/85
ATTACH #5 PAGE 15/25



SCENARIO No. 3: 1CS+2LH+2HH WITH MAX SPRAY PH ASSUMPTIONS

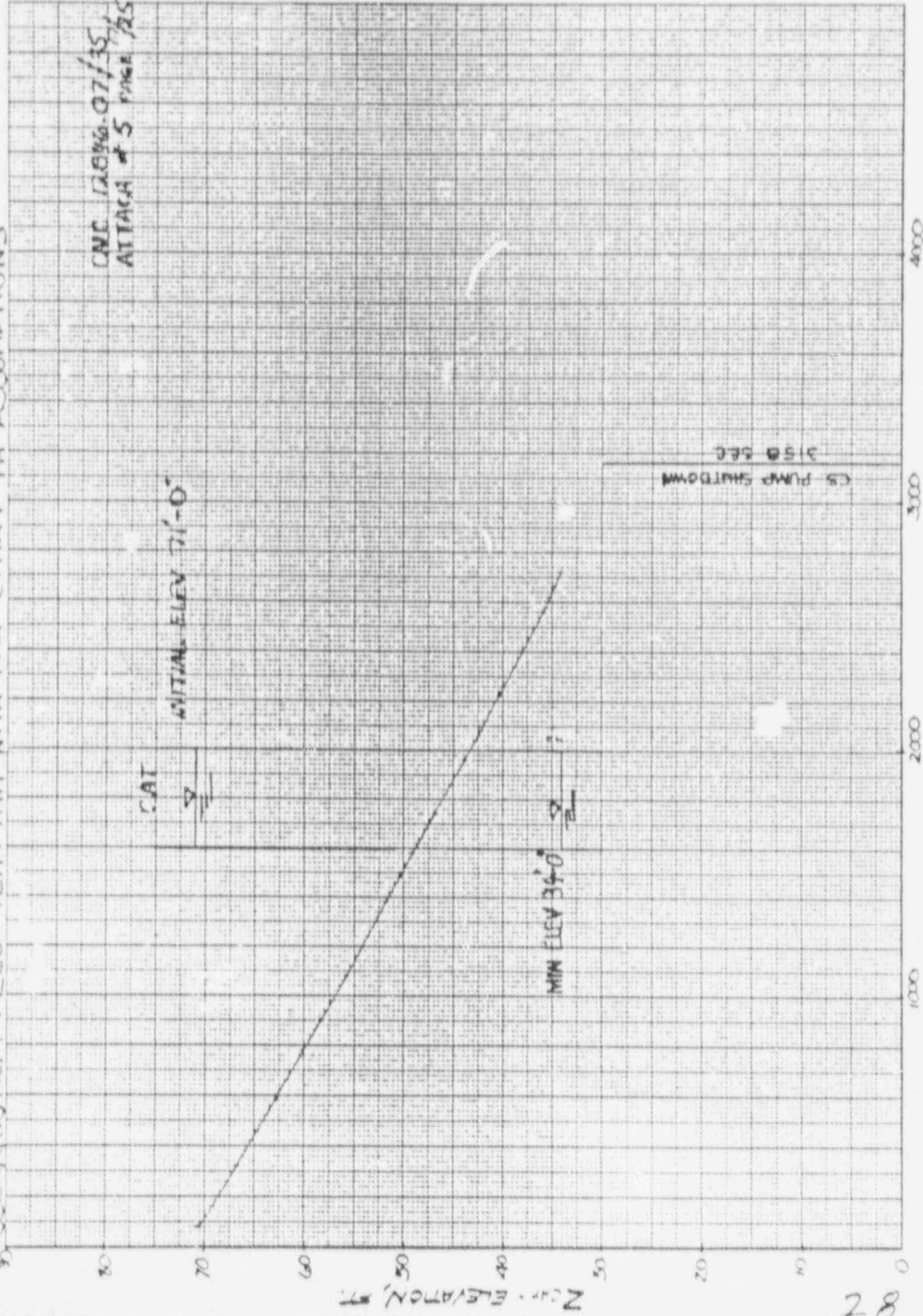


CNC 12846.07/35
ATTACH #5 PAGE 16/25

LZ

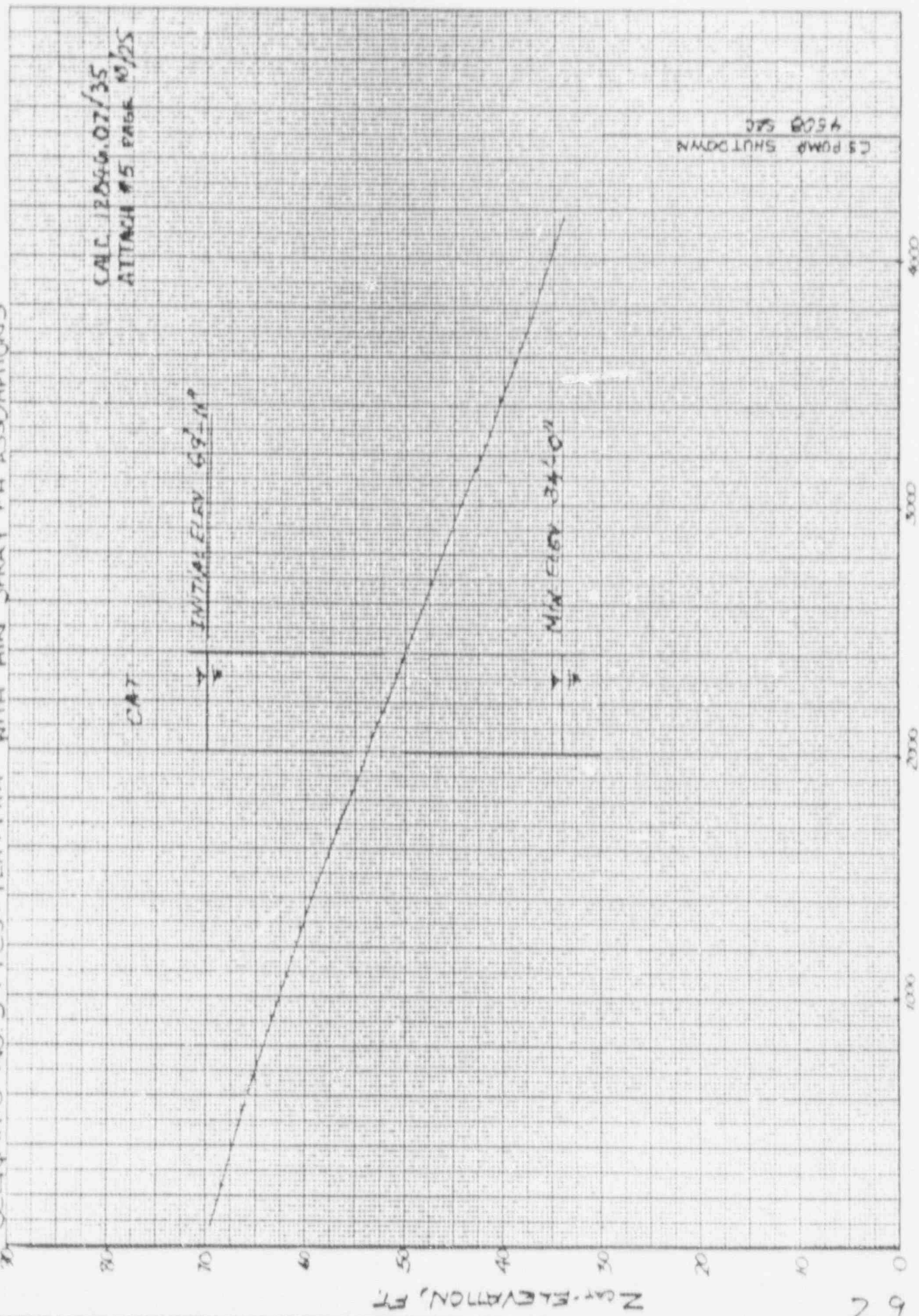
PREPARED BY: [Signature] 6/2/80
CHECKER: F. ONEIL 5 JUNE 80

SCENARIO No. 4 : 2CS + 1LH + 1HH WITH MAX SPRAY PH ASSUMPTIONS



PREPARED BY: C. LINTHROP 11/7/80
CHECKER: P. ONEIL 5 JUNE 80

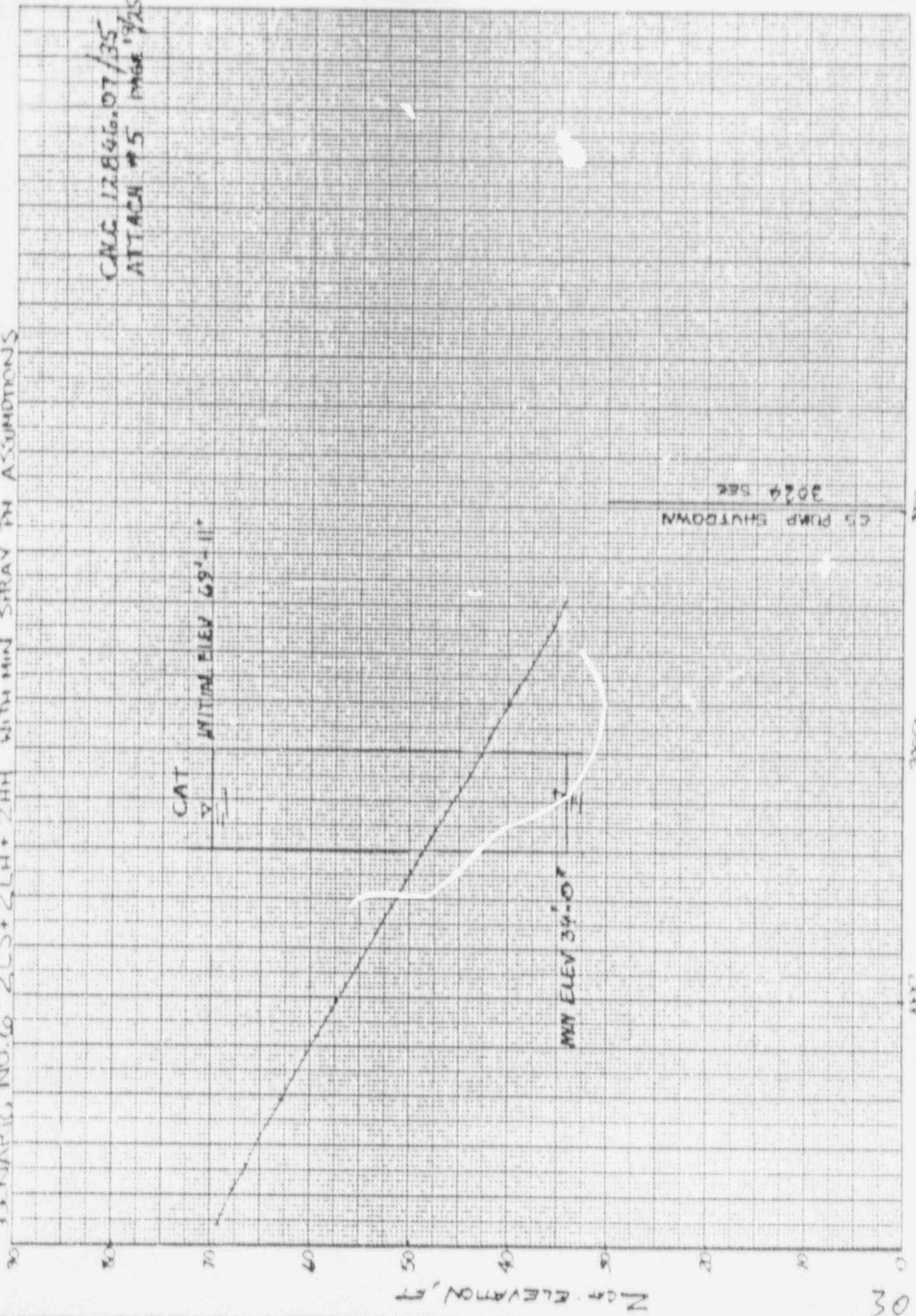
SCENARIO NO. 5: 1CS + 1LH + 1HH WITH MIN SPRAY TH ASSUMPTIONS



PREPARED BY: [Signature] 10/1/80
CHECKER: P. ONEIL 5 JUNE 80

CALC 12846.07/35
ATTACH #5 PAGE 19/25

SECTION NO. 6 - 2 CS + 2 LH + 2 HH WITH MIN STRAY IN ASSUMPTIONS



CS PUMP SHUTDOWN 3024 SEC

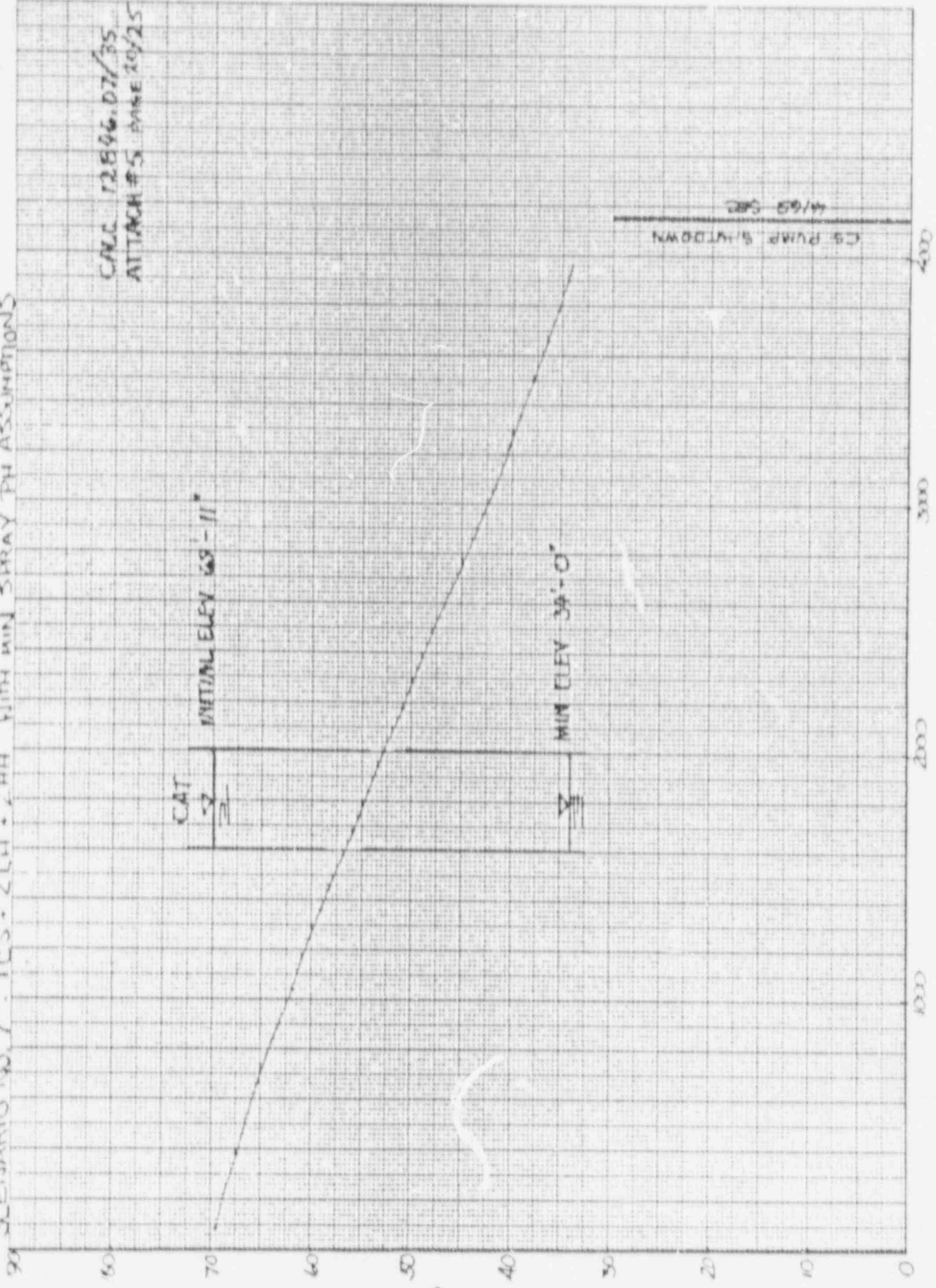
CAT INITIAL ELEV 69'-11"

MIN ELEV 34'-10"

PREPARED BY: EASTMAN W/S/RO
CHECKER: P. ONEIL 5/29/80

SCENARIO No. 7 : 1CS + 2LH + 2HH HIGH MIN SPRAY PH ASSUMPTIONS

CALL 12896.07/35
ATTACH #5 PAGE 20/25



CAT
INITIAL ELEV 69'-11"

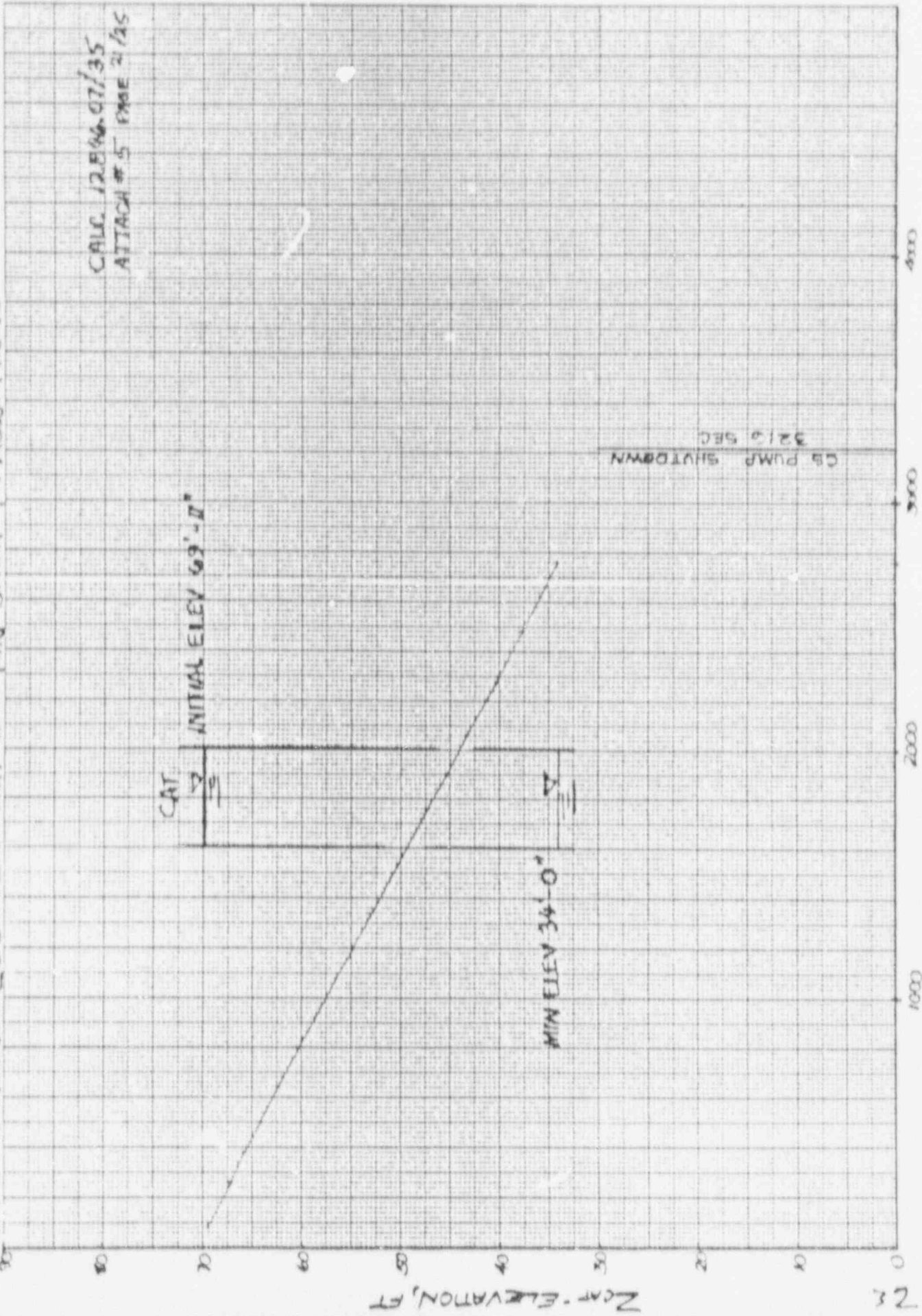
MIN ELEV 34'-0"

CS PUMP SHUTDOWN
4/68 SEC

PREPARED BY: C. BARTHOLOMEW 6/3/80
CHECKER: P. ONIEN 5 JUNE 80

SCENARIO NO. 8: 2CS + 1LH + 1HH WITH MIN SPRAY PH ASSUMPTIONS

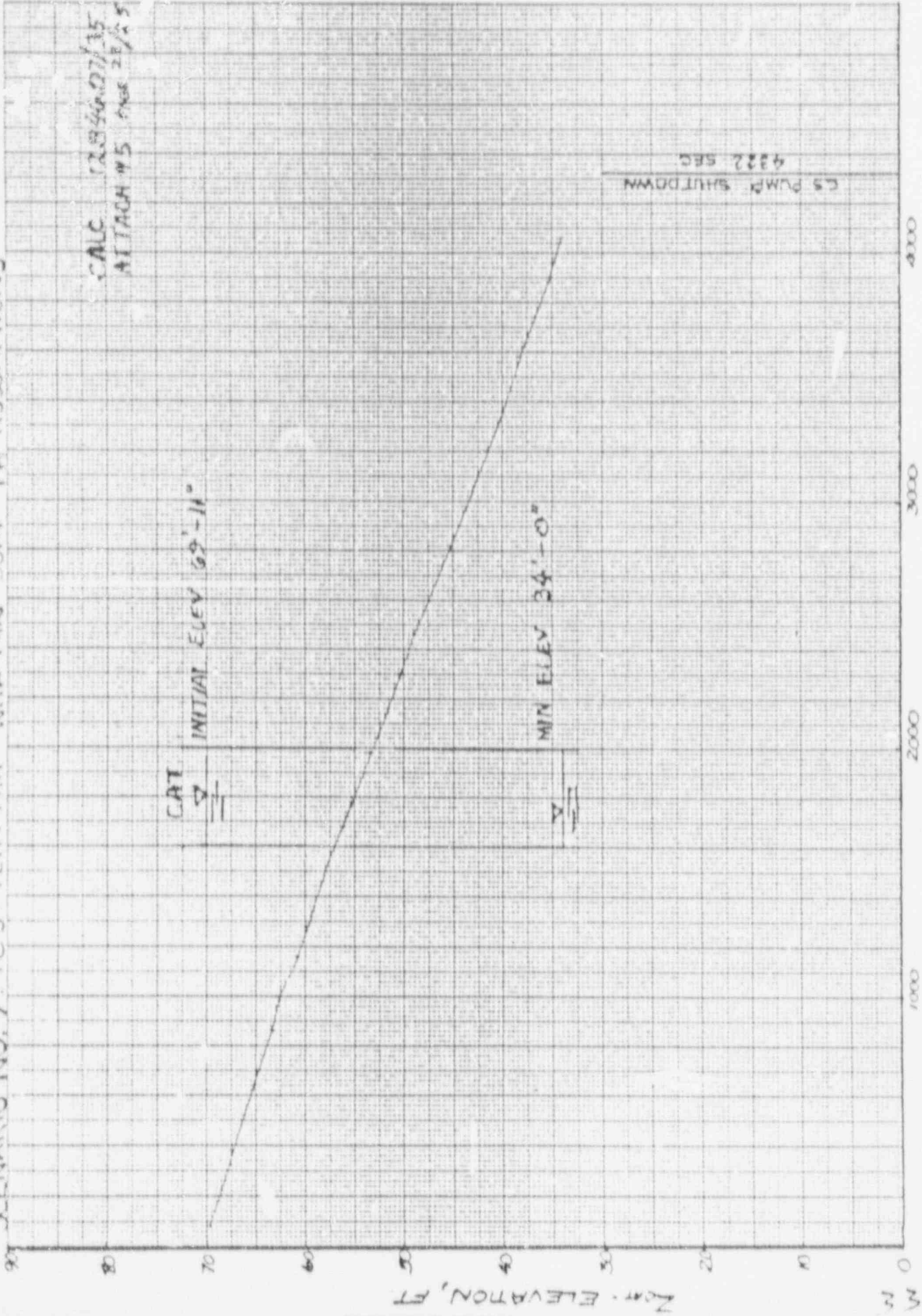
CALC. DATE: 6/7/85
ATTACH # 5 PAGE 2/25



PREPARED: C. B. Bennett 6/3/83
CHECKER: P. O'NEIL 5 JUNE 80

SCENARIO No. 9: ICS + IHH + IHH WITH MIN SUMP PH ASSUMPTIONS

CALC 128940.07/35
ATTACH #5 PAGE 28/25



CAT

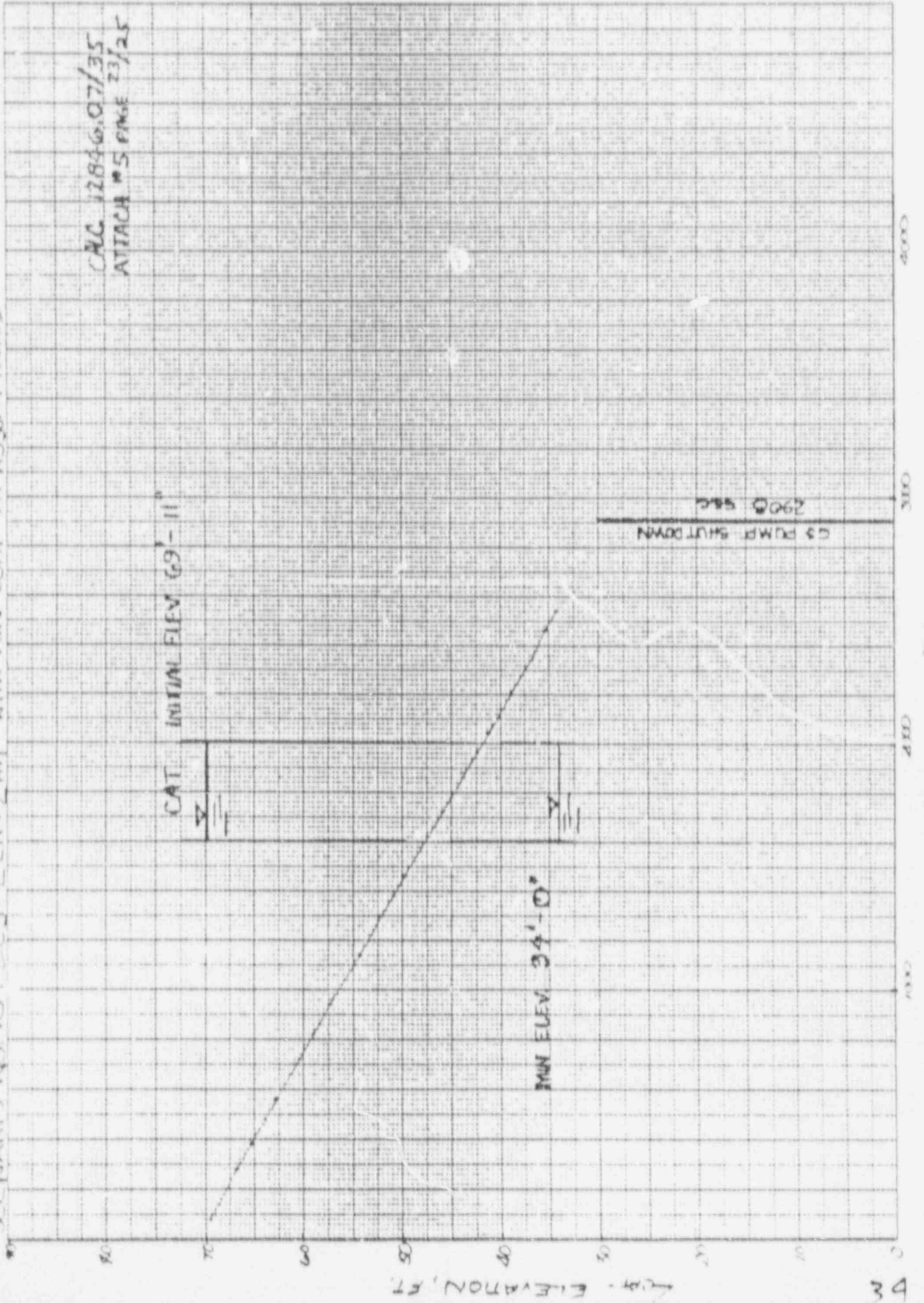
INITIAL ELEV 69'-11"

MIN ELEV 34'-0"

CS PUMP SHUTDOWN 4222 SEC

DRAWN BY: C. J. [unclear] 6/24/10
CHECKER: P. ONEIL 5 JUNE 10

SCENARIO No. 10: 20S + 2LH + 2HH WITH MIN SUMP PH ASSUMPTIONS

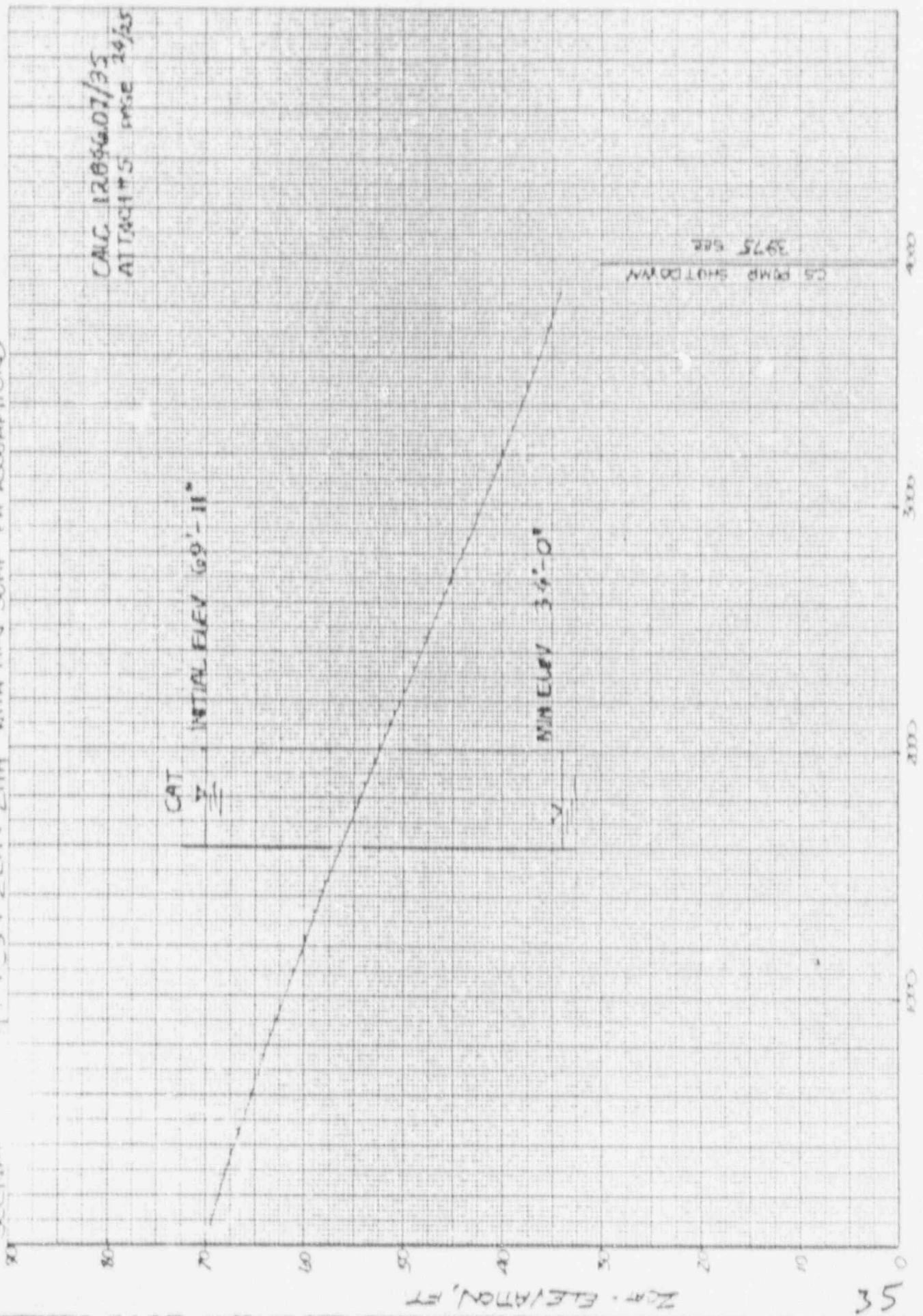


CAC 12846.07/35
ATTACH #5 PAGE 23/25

PREPARED BY: C. T. ... 6/23/80
CHECKER: P. ONEIL 5 JUNE 80

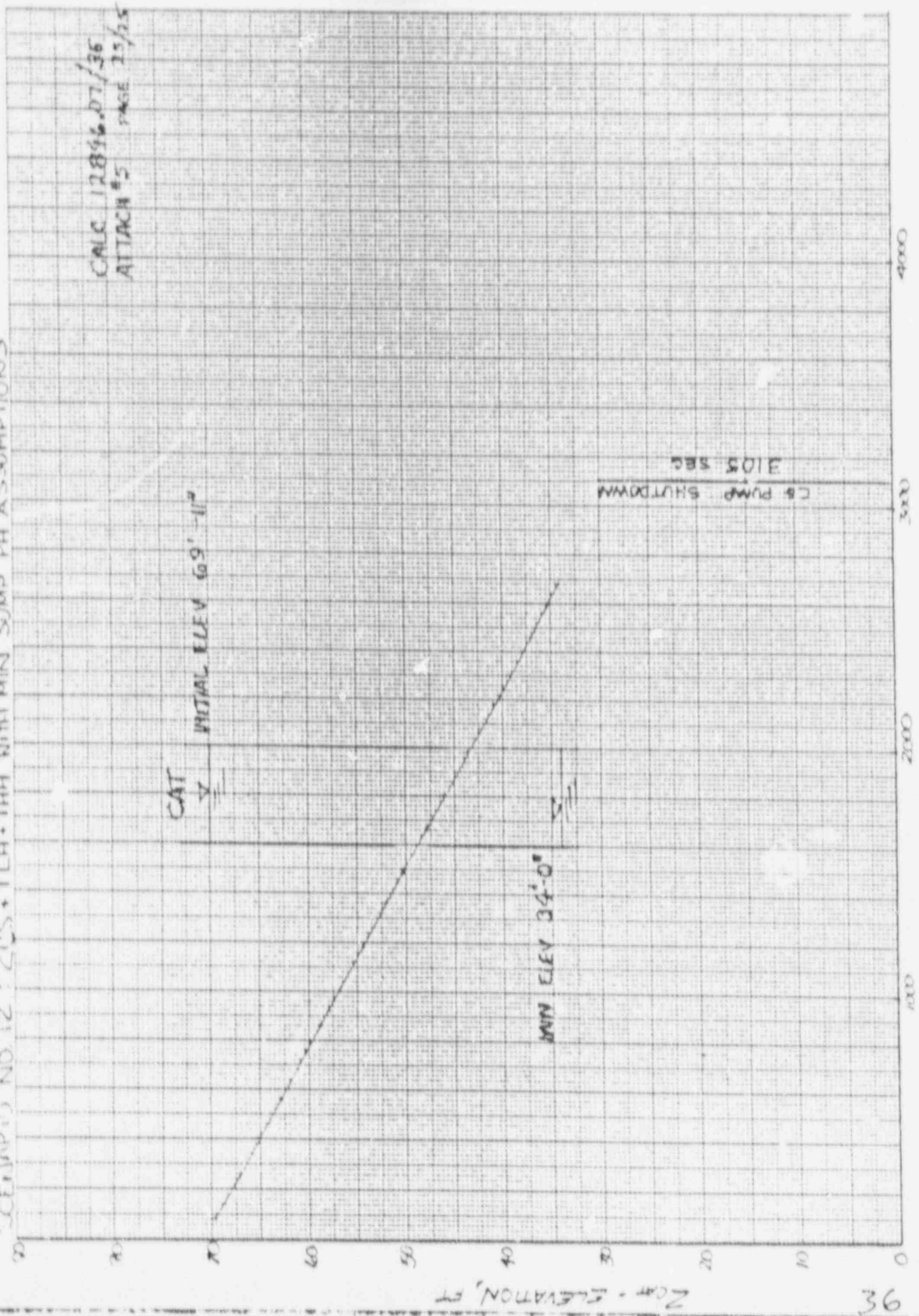
SCENARIO 1: 1CS + 2LH + 2HH WITH MIN SUMP PH ASSUMPTIONS

CALC. 1209607/85
ATTACHED: MSE 14/85



DRAWN: C. FLETCHER 6/3/80
CHECKER: F. O'NEIL 5/30/80

SCENARIO NO. 12: 20S + 1 LH + 1 HH WITH MIN SUMP PH ASSUMPTIONS



CALC 12896.DT/36
ATTACH #5 PAGE 25/35