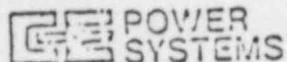


7/6/83

GPU 2425

C-E Power Systems
Combustion Engineering Inc.
1000 Prospect Hill Road
Windsor, Connecticut 06095

Tel. 203/561-1211
Telex 90297



CONFIDENTIAL
COUNSEL ONLY

Enclosure (1) provides generic design differences between a typical C-E operating plant and B&W Three Mile Island Unit 2 (TMI). We are providing this material as background, knowing of your need to respond to regulatory inquiries. Since this information is generic and was gathered from services at Windsor, we recommend that you check the specific validity with respect to your unit.

Part a of Enclosure (1) provides a listing of design features of C-E operating plants which would tend to mitigate an event similar to the Loss of Feedwater Event which occurred at TMI. Such design features in conjunction with improved operating and emergency procedures will give confidence that an incident similar to the TMI event has a very low probability of occurrence at a C-E assigned operating unit. C-E will continue to evaluate pertinent design features and promptly recommend any design modifications and/or procedural changes which enhance operating plant safety.

Part b of Enclosure (1) provides system descriptions which form the basis for the conclusions stated in Part a. Part c of Enclosure (1) provides a C-E engineering evaluation of the sequence of events which would transpire if an event similar to the TMI Loss of Feedwater incident were to occur on a C-E operating plant. Part c of Enclosure (1) is a generic description of expected C-E plant response to events similar to those experienced at TMI.

Combustion Engineering stands ready to assist you in responding to I.E. Bulletin 79-05. If you should require such assistance from C-E, please contact me.

Sincerely,

A handwritten signature in black ink, appearing to read "Pletzner" or "Pletzner, W. H. Krause".

Manager, Engineering Services

PWN:mtm

ENCLOSURE (1)

C-E/B&W

PRELIMINARY GENERIC PLANT COMPARISON

The information presented in this enclosure is based on preliminary information concerning the nuclear incident at Three Mile Island Nuclear Power Plant Number 2. The results stated in this enclosure are based on C-E engineering judgement of events which transpired during the accident. The information and material discussed and presented by C-E with respect to the Three Mile Island Nuclear Power Plant design has been obtained from the Preliminary and Final Safety Analysis reports and personal knowledge.

GENERIC DESIGN FEATURES WHICH DIFFER BETWEEN C-E AND TMI-2

DESIGN FEATURE

COMMENT

a) C-E plants have a low steam generator water level RPS trip. For a loss of feedwater, BWH plants trip on high primary system pressure. The BWH trip signal also lifts the pressurizer relief valves.

The combination of a low steam generator water trip and higher steam dump capacity prevent significant primary system pressure excursions on C-E plants.

b) C-E plants have 40% steam dump/turbine bypass capacity. BWH plants have 15% steam dump/turbine bypass capacity.

There is more time available to establish emergency feedwater after loss of main feedwater in the C-E system and less likelihood of lifting a primary relief valve.

C-E steam generators have a larger secondary water inventory than the TMI steam generators.

Only 20-25% of RCS fluid is needed to cover C-E core vs 40-45% of RCS fluid for TMI.

C-E core elevation is relatively lower in the NSSS layout than TMI core.

A significant fraction of the TMI RCS fluid, once there is void in the RCS, will collect in the steam generator/cold leg loop seal.

C-E steam generator elevation does not form a cold leg loop seal.

The higher elevations result in a better potential to initiate and maintain natural circulation.

C-E steam generator elevation is higher than TMI steam generator.

U-tube steam generator design allows reflux condensation of RCS fluid in hot leg vs only cold leg return of condensed RCS fluid for OTSG design. U-tube steam generator also allows more water inventory.

C-E U-tube steam generator design vs TMI once through straight tube (OTSG) design.

There is more potential for water retention in the TMI SGs with consequent unavailability of the water to cool the core.

TMI steam generators have more primary side water inventory than the C-E steam generators.

A surge line loop seal allows water or two-phase fluid retention in the pressurizer with the primary system voided. This will produce an indication that the reactor vessel is not voided based on a false pressurizer level indication. The C-E system without the surge line loop seal is less susceptible to this false indication.

The TMI design has a loop seal in the pressurizer surge line. The C-E design has no loop seal.

DE-1001 ELEVATION

9. The C-E pressurizer is at a higher elevation than the TMI pressurizer.
10. The C-E HPSI shutoff head is lower than the TMI HPSI shutoff head.

C-E HPSI

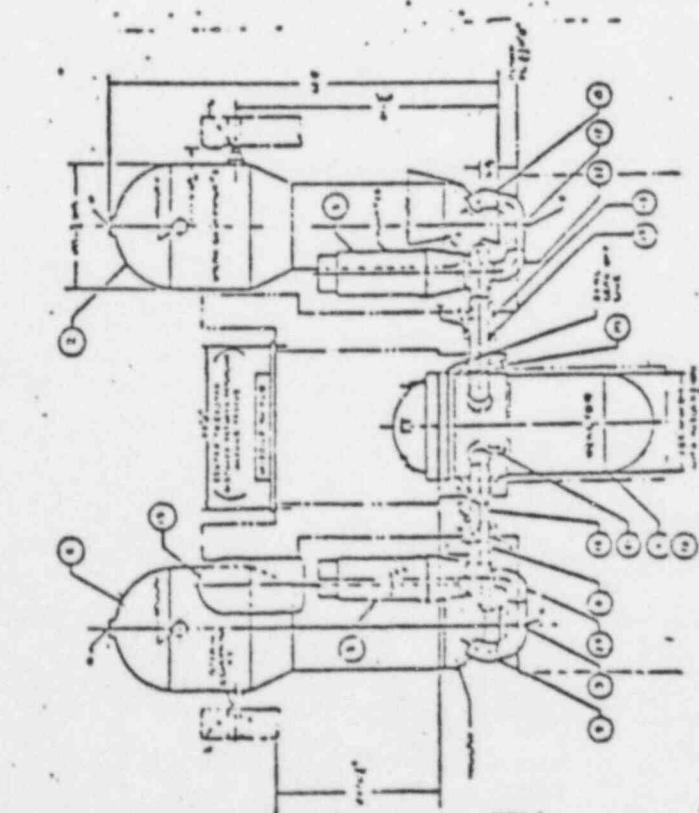
The increased elevation increases the likelihood of draining the pressurizer when the hot leg is voided.

The lower shutoff head will not result in lifting the pressurizer relief or safety valves if the HPSI pumps are left on.

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Fig. 1 b

B & W Three Mile Island



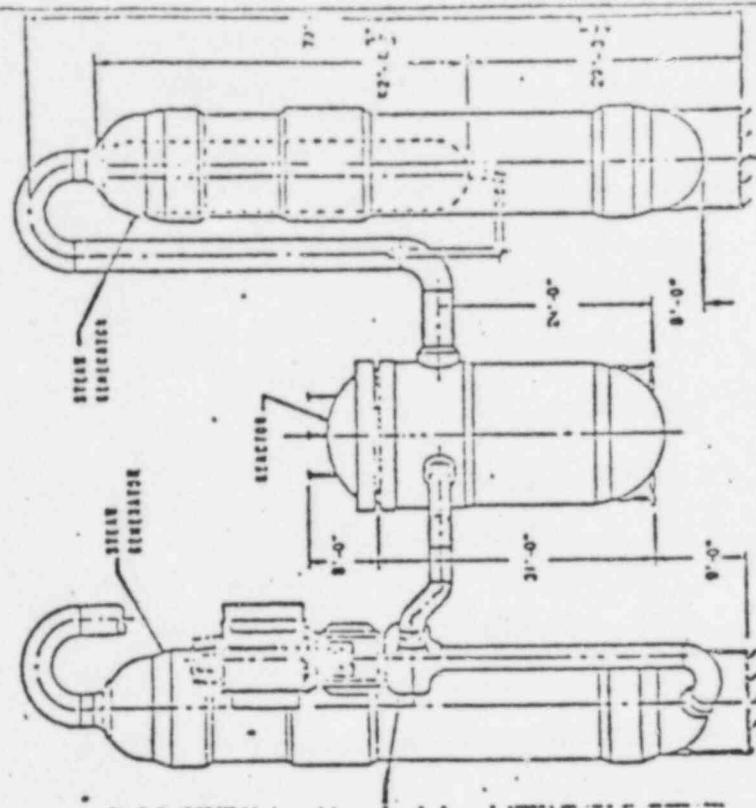
Core Power
System Pressure
Total Reactor Flow

	Reactor Vessel	Steam Generator	Pressure Vessel	Other	Total
Core Power	3632 ft ³	220 ft ³	2633 ft ³	1563 ft ³	7558 ft ³
System Pressure	250 psig	250 psig	250 psig	250 psig	250 psig
Total Reactor Flow	1513 ft ³ /s	911 ft ³ /s	1513 ft ³ /s	1513 ft ³ /s	5047 ft ³ /s

Reactor Coolant Volume

	Reactor Vessel	Steam Generator	Pressure Vessel	Other	Total
Core Power	2772 ft ³	910 ft ³	4564 ft ³	910 ft ³	8100 ft ³
System Pressure	250 psig	250 psig	250 psig	250 psig	250 psig
Total Reactor Flow	1513 ft ³ /s	911 ft ³ /s	1513 ft ³ /s	1513 ft ³ /s	5047 ft ³ /s

	Reactor Vessel	Steam Generator	Pressure Vessel	Other	Total
Core Power	2772 ft ³	910 ft ³	4564 ft ³	910 ft ³	8100 ft ³
System Pressure	250 psig	250 psig	250 psig	250 psig	250 psig
Total Reactor Flow	1513 ft ³ /s	911 ft ³ /s	1513 ft ³ /s	1513 ft ³ /s	5047 ft ³ /s



Core Power
System Pressure
Total Reactor Flow

	Reactor Vessel	Steam Generator	Pressure Vessel	Other	Total
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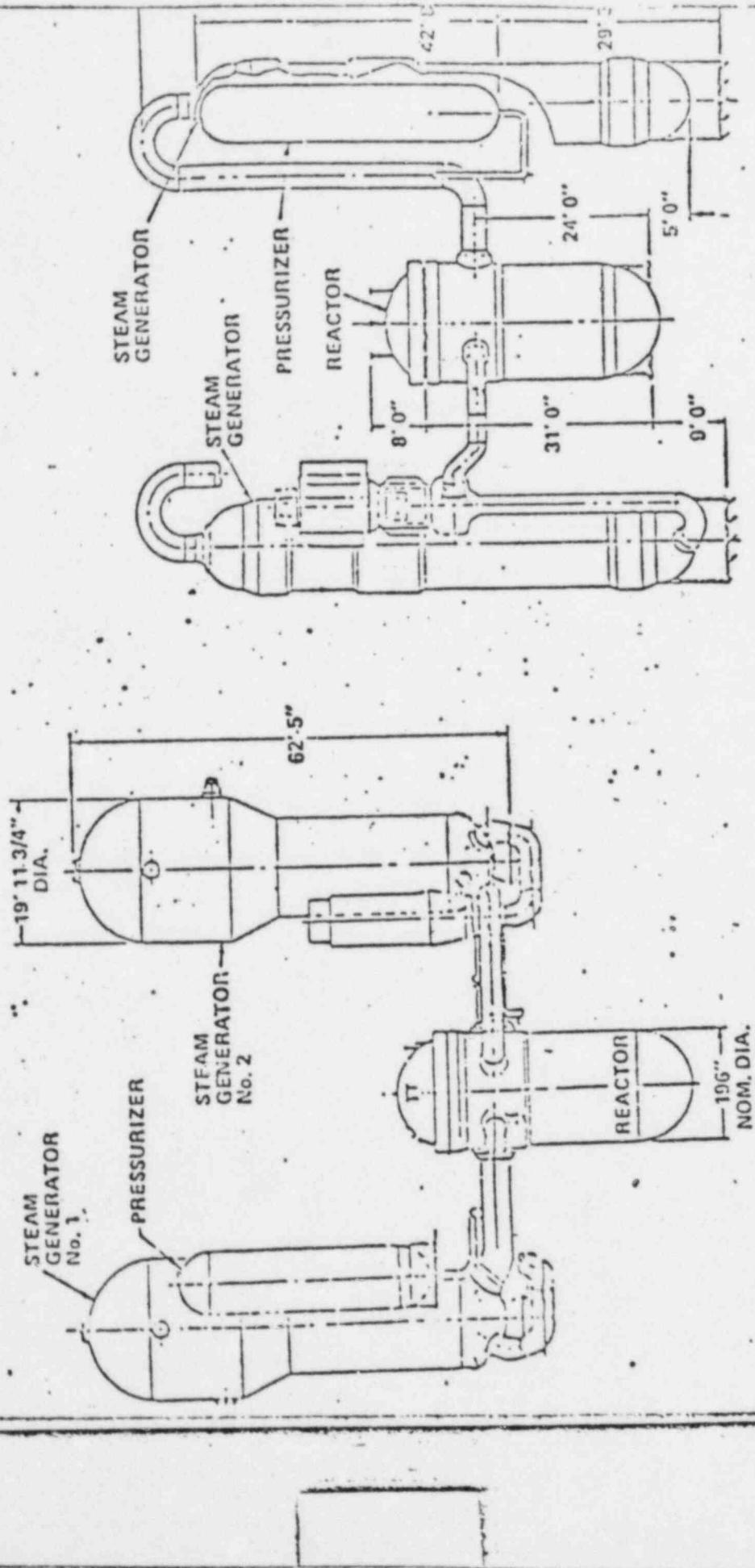
	Reactor Vessel	Steam Generator	Pressure Vessel	Other	Total
Core Power	2772 ft ³	910 ft ³	4564 ft ³	910 ft ³	8100 ft ³
System Pressure	250 psig	250 psig	250 psig	250 psig	250 psig
Total Reactor Flow	1513 ft ³ /s	911 ft ³ /s	1513 ft ³ /s	1513 ft ³ /s	5047 ft ³ /s

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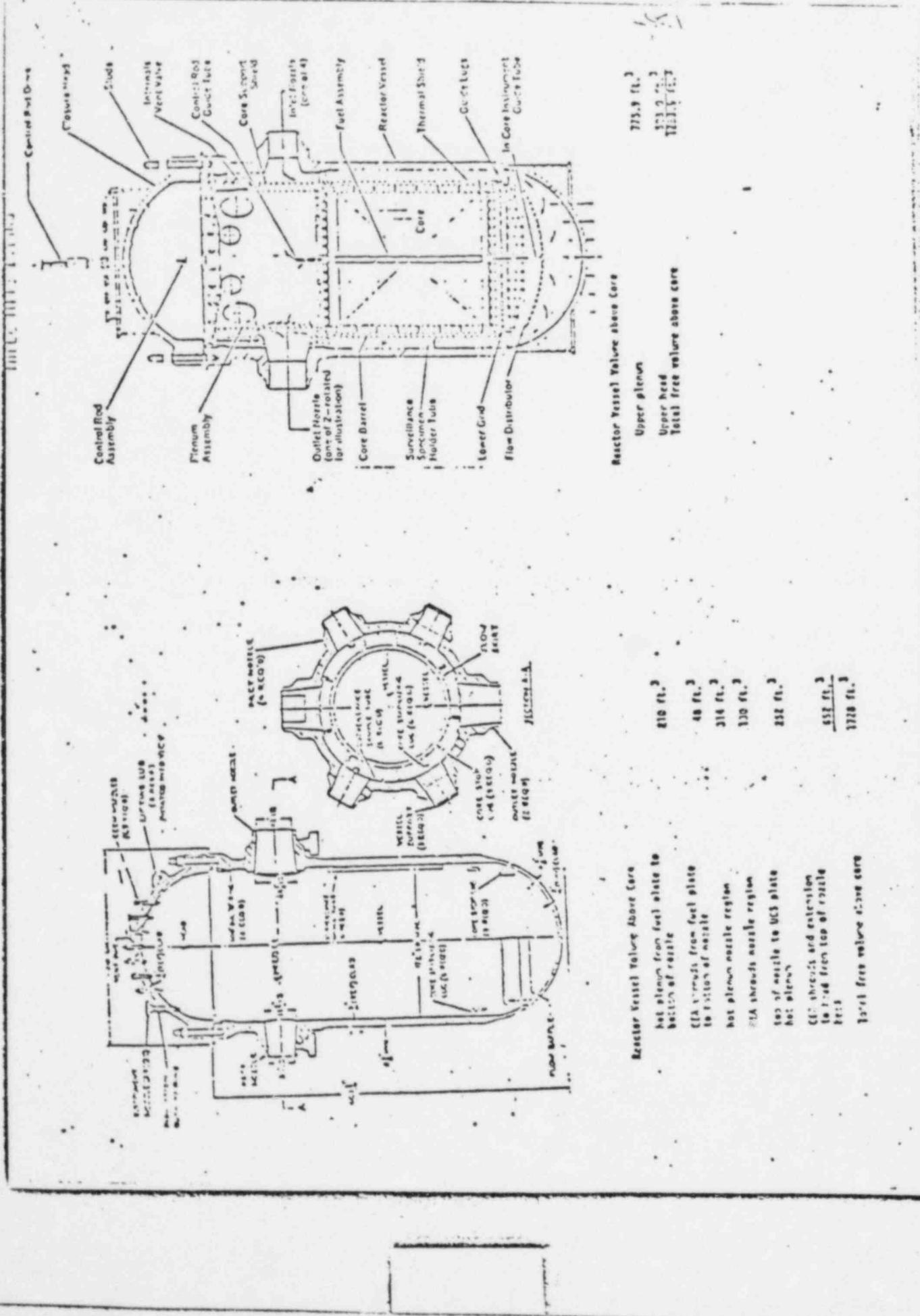
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C.E.

D&W
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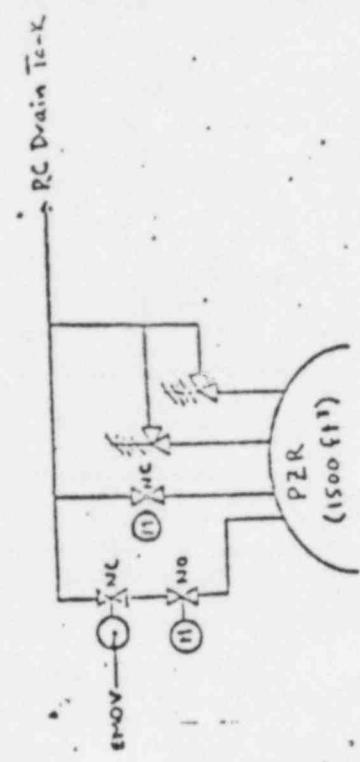


NOTE: DRAWN TO SCALE RELATIVE SCALE



CC → Quench Tank

BW
Three Mile Island



Quench Tank (B & W "PC Drain Tank")

Setting 650 psig/503 °F.
Volume 1000 cu ft.

Normal 1 { } 317,000 l/hr. @ 515 psig
Relief 1 { } 347,000 l/hr. @ 515 psig

PC

Cooler Tank
Setting 100 psig/250 °F
Normal 1 reliters @ 1133 hr. 3

1234
Normal 131,522 l/hr. (min)
Relief Solenoid Operate

Table 1
Normal 215,222 l/hr. No accumulation
Relief Capacity 215,222 l hr. No freezing limited
Type 1
Size 1
Steel 1 inches

Quench Tank (B & W "PC Drain Tank")
Setting 650 psig/503 °F.
Volume 1000 cu ft.
Normal 1 { } 317,000 l/hr. @ 515 psig
Relief 1 { } 347,000 l hr. @ 515 psig

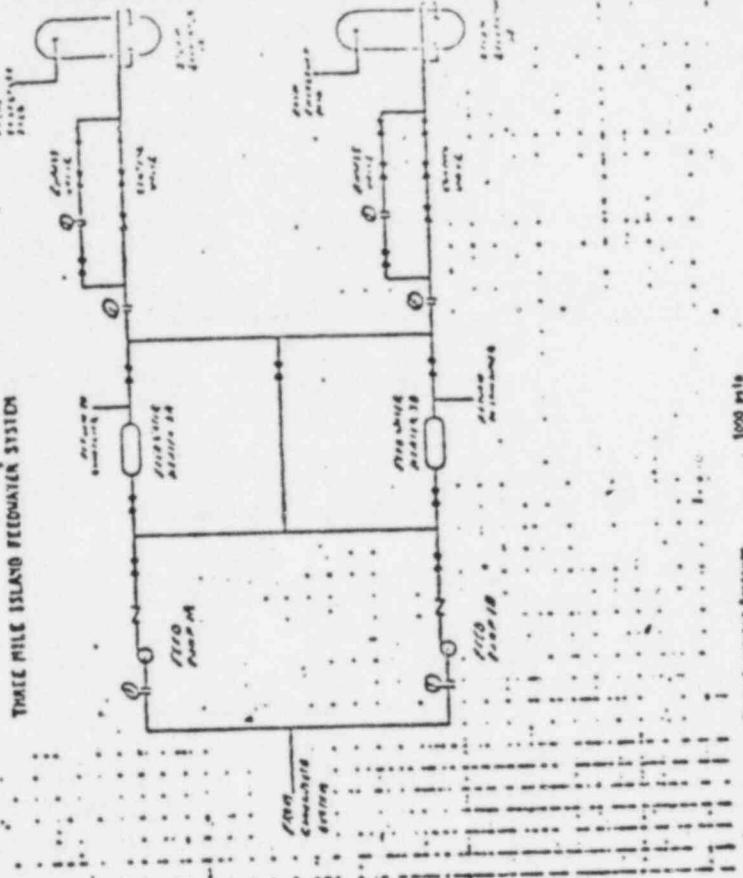
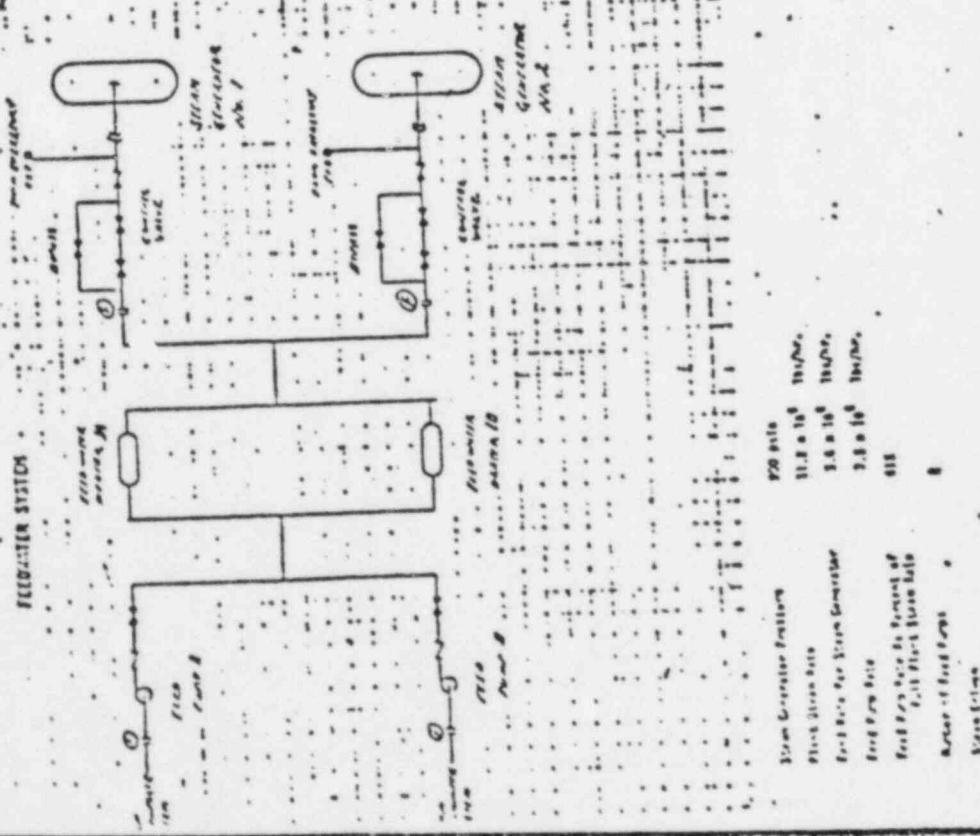
PC

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Setting 650 psig/503 °F.
Volume 1000 cu ft.

Normal 1 { } 317,000 l hr. @ 515 psig
Relief 1 { } 347,000 l hr. @ 515 psig

Quench Tank (B & W "PC Drain Tank")
Setting 650 psig/503 °F.
Volume 1000 cu ft.

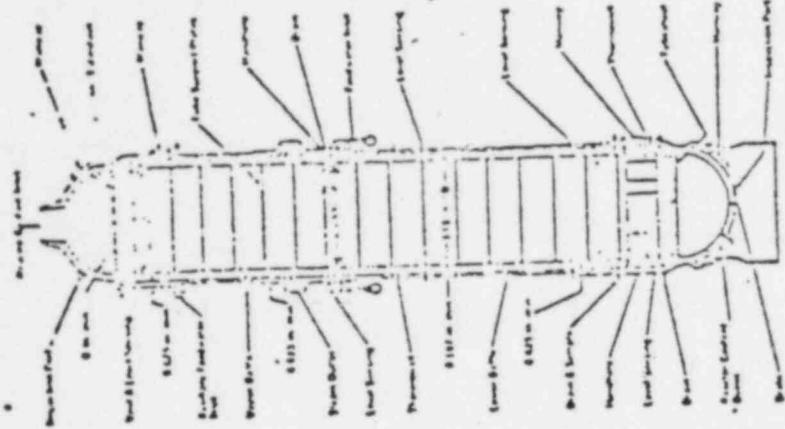
Normal 1 { } 317,000 l hr. @ 515 psig
Relief 1 { } 347,000 l hr. @ 515 psig



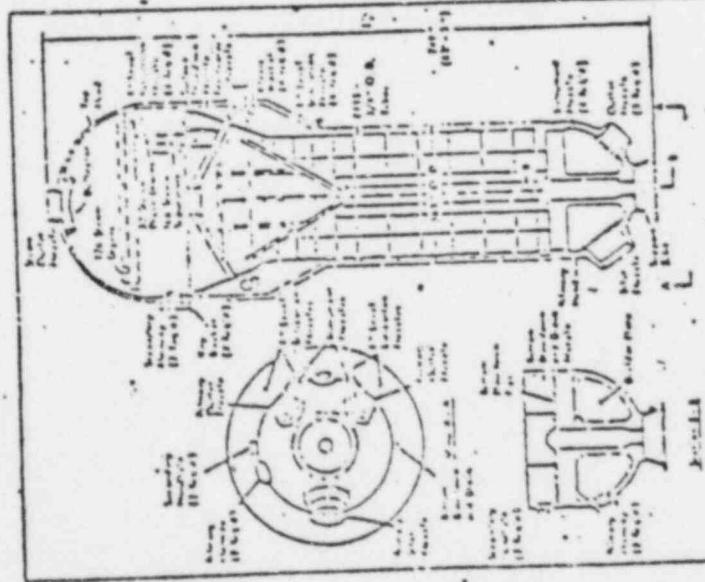
<i>Brian Grouse Prey</i>	1000 ptlts
<i>Plant Stem Buds</i>	1.1×10^3
<i>Food Hair for Brian Grouse</i>	6.0×10^4
<i>Food Buds</i>	6.0×10^4
<i>Food Buds or Foment of Fall Final State Buds</i>	\$1.1
<i>Foment of Fall Final State Buds</i>	\$1.1
<i>Brian Grouse</i>	\$1.1

CE

U.S.A. Three Little Island



Three Little Island



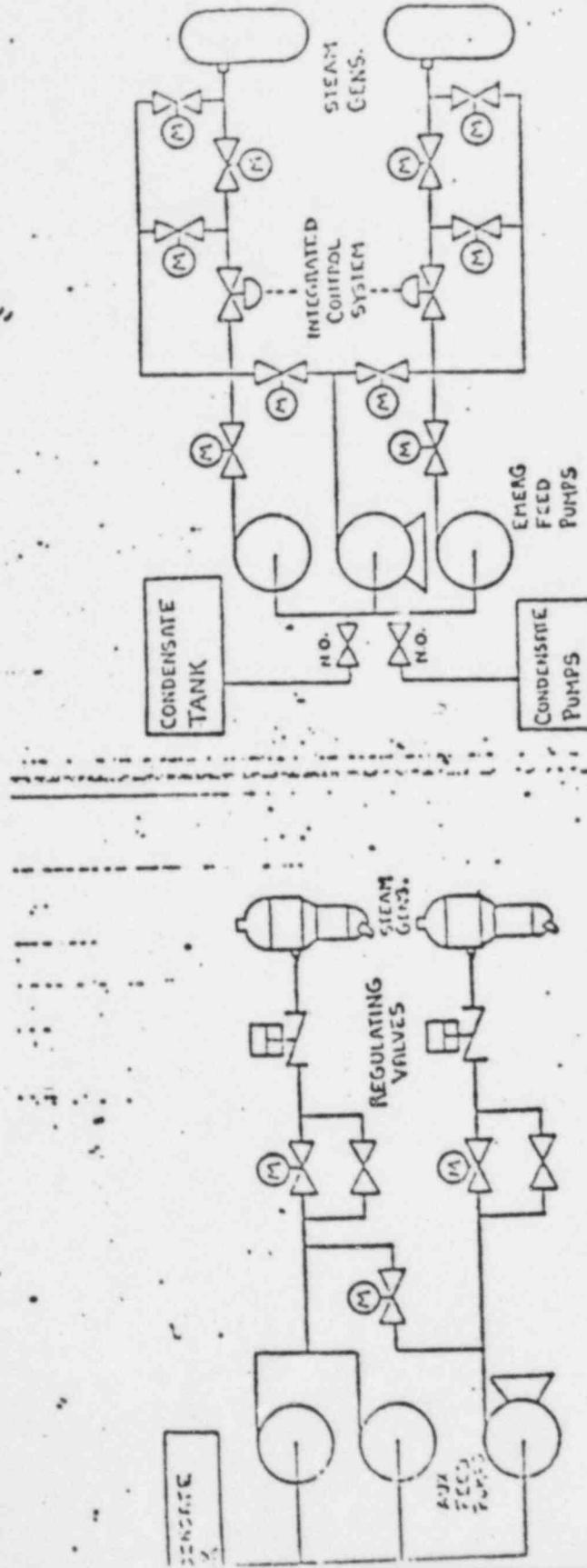
Three Little Islands

Variable	Value	Source
Water temperature, south, March	52.0 ± 0.5°	Estimated
Water temperature, north, April	52.0 ± 0.5°	Estimated
Water temperature, south, May	53.0 ± 0.5°	From climatic lot 8 (original) each, Rep.
Water temperature, south, June	54.0 ± 0.5°	Estimated
Water temperature, south, July	55.0 ± 0.5°	Estimated
Water temperature, south, August	56.0 ± 0.5°	Estimated
Water temperature, south, September	57.0 ± 0.5°	Estimated
Water temperature, south, October	58.0 ± 0.5°	Estimated
Water temperature, south, November	59.0 ± 0.5°	Estimated
Water temperature, south, December	60.0 ± 0.5°	Estimated

Variable	Value	Source
Nature of soil	Soil A	1
Rock transfer rate, south, March	0.010 ± 0.005	Estimated
Velocity, 2.0	1.12 ± 0.12 m/sec	Estimated
Rock transfer rate, April, 3.0	0.012 ± 0.005	Estimated
Rock transfer rate, May, 4.0	0.013 ± 0.005	Estimated
Rock transfer rate, June, 5.0	0.014 ± 0.005	Estimated
Rock transfer rate, July, 6.0	0.015 ± 0.005	Estimated
Rock transfer rate, August, 7.0	0.016 ± 0.005	Estimated
Rock transfer rate, September, 8.0	0.017 ± 0.005	Estimated
Rock transfer rate, October, 9.0	0.018 ± 0.005	Estimated
Rock transfer rate, November, 10.0	0.019 ± 0.005	Estimated
Rock transfer rate, December, 11.0	0.020 ± 0.005	Estimated

E 2 E 2 E 2

Three Mile Island



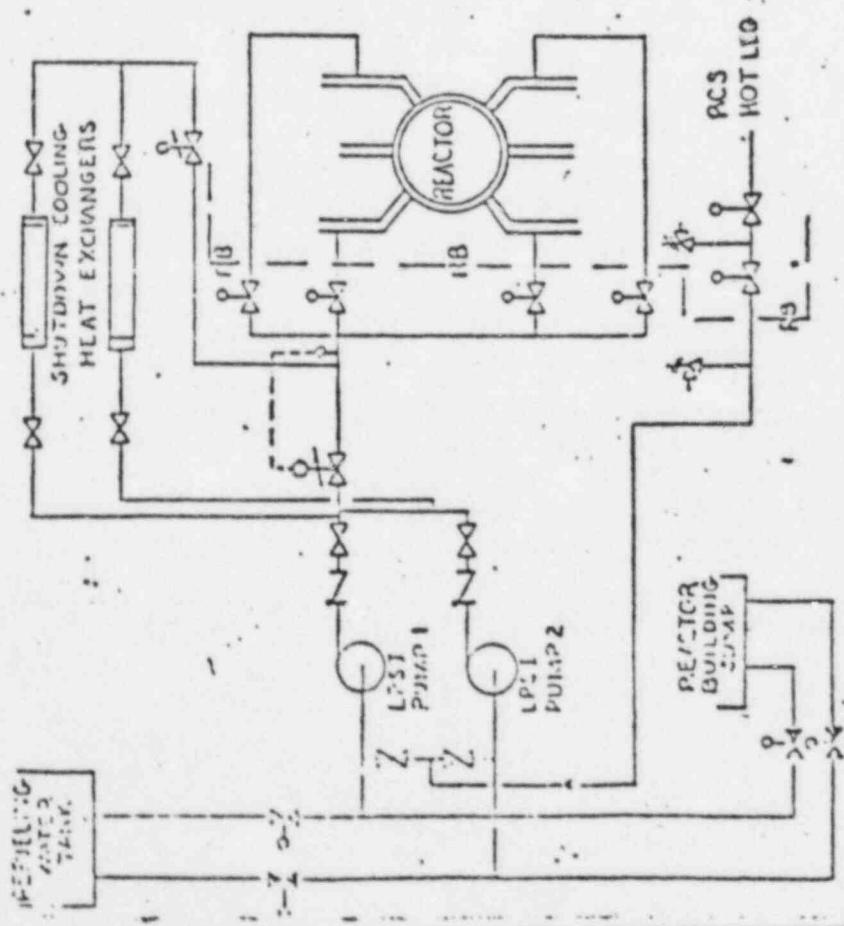
EMERGENCY FEED PUMP

CONTROLLER BY	LCV OF PL. GCV'S LCV OF ESD PL. RELAY'S PULLS LCV FIELD-SIDE CIRCUITUAL PRESSURE
EMERGENCY FIELD PUMP	1. UPLINE PULLIN 2. FLOW DRAIN
CAPACITY	100% REACTOR HEAT 50% REACTOR HEAT (L.C.W.)
SOURCES OF SUCTION	CO-GENERATE PULLS (IF OPERATING) G.G. GEN. SOURCE TANKS
EMERGENCY POWER	115 230VAC
NOT NEEDED	YES
NUMBER OF POSITION	2 POSITION
NUMBER OF PUMP	2 PUMPS
NUMBER OF TANK	2 TANKS

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E

LL

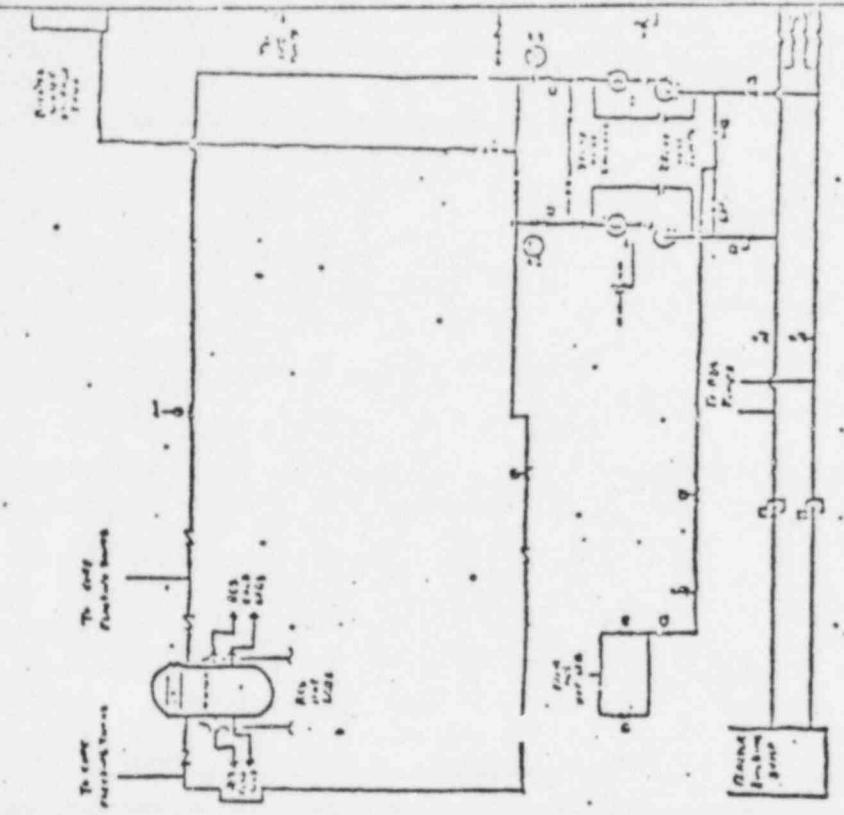
U & W
Three Mile Island



Shutdown Cooling Initiation Temperature
Temperature, °F
Pressure, psig
Design Basis

Initiation Cooling Initiation Temperature
Temperature, °F
Pressure, psig
Design Basis

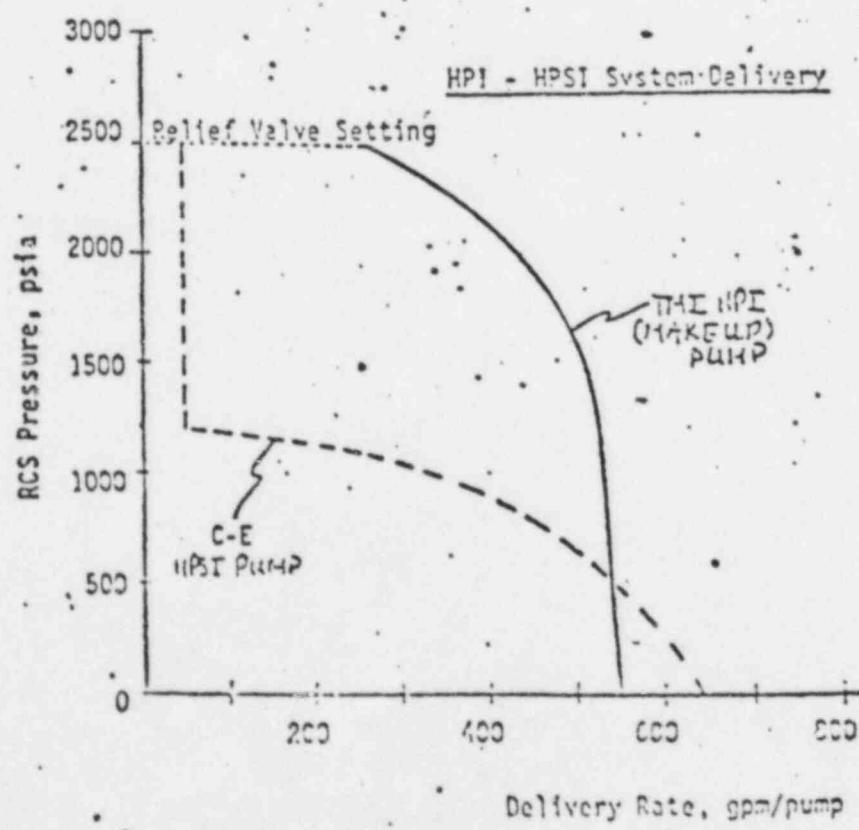
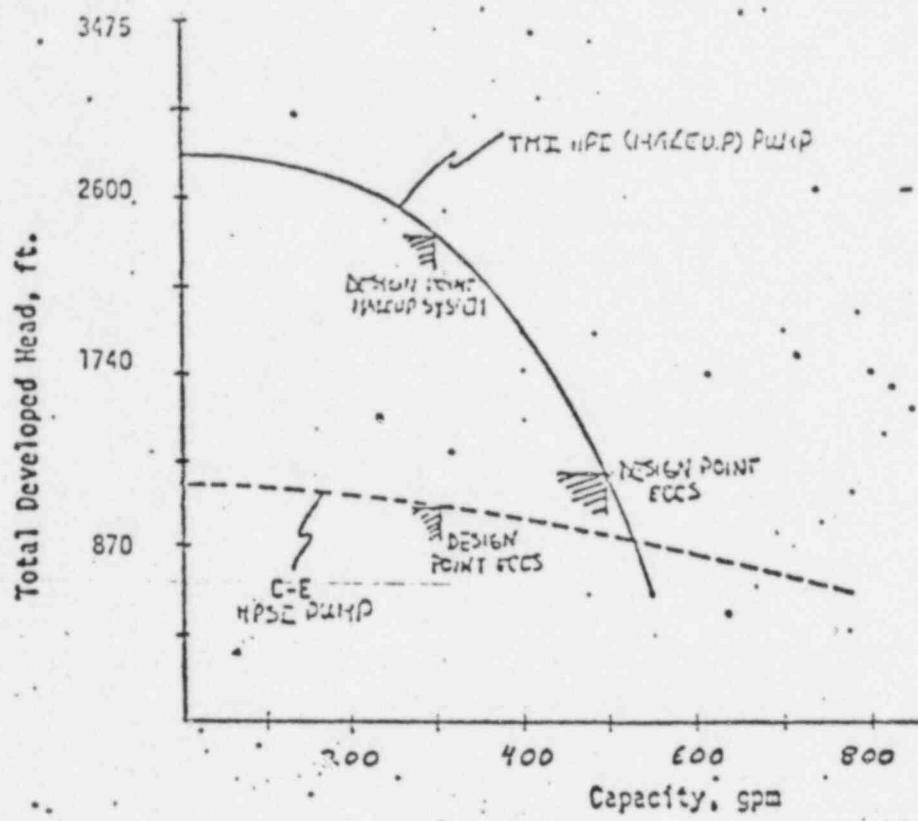
Cool down RCS from 210 °F to 140 °F in 14 hours, starting
7 hrs after shutdown.

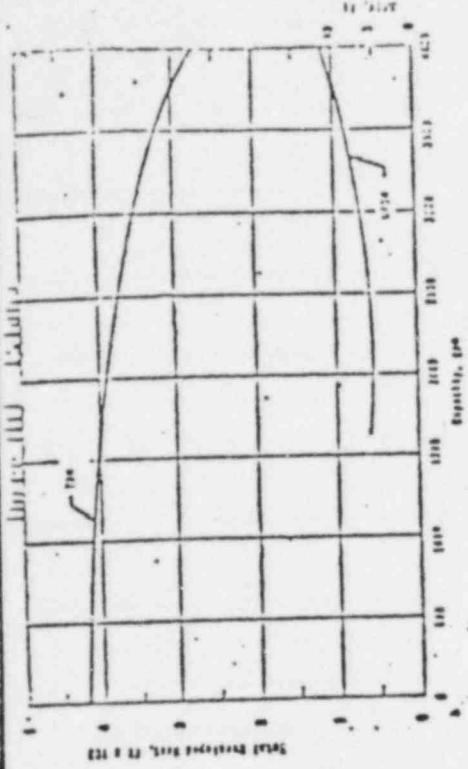


Shutdown Cooling Initiation Temperature
Temperature, °F
Pressure, psig
Design Basis

Cool down RCS from 210 °F to 140 °F in 14 hours, starting
7 hrs after shutdown.

E 2 6 2





Low Pressure Safety Injection Pump

Low Pressure Safety Injection Pump

Quantity	2
Type	Single stage, vertical centrifugal
Quality group class	AFC III, Class 2
Design pressure	312.5 psig
Design temperature	450°F
Design fluid/solid	Water
Materials	Stainless steel
Piston/pumpcase	316L SS
Shaft	316L SS
Piping	316L SS

Shuttle Cooling Plant Exchange
Shell and tube, horizontal.
Tube side:

Fluid: Deionized water
Design pressure: 150 psig
Design temperature: 200°F

Tube side:

Fluid: Deionized water
Design pressure: 150 psig
Design temperature: 200°F

Shell side:

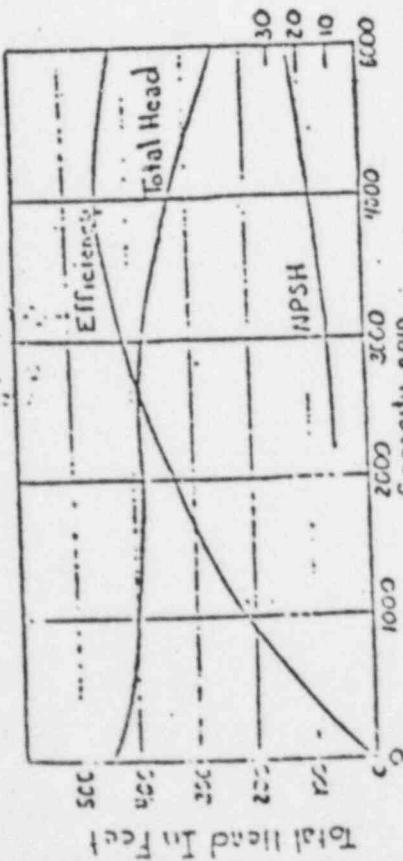
Fluid: Deionized water
Design pressure: 150 psig
Design temperature: 200°F

Design cases:

Corporant cooling water
150 psig
123°F
Carbon Steel

Design cases:

Take side temperatures
Shell side temperature
123°F
123°F
Carbon Steel



Shuttle Cooling System Component Data

Deep Well Removal Pump

Quantity	2
Type	Single stage, vertical centrifugal
Quality group class	AFC III, Class 2
Design pressure	312.5 psig
Design temperature	450°F
Design fluid/solid	Water
Materials	Stainless steel
Piston/pumpcase	316L SS
Shaft	316L SS
Piping	316L SS

Decay Heat Removal Coolers

Quantity	2
Type	Shell and tube
Tube side:	442.2 ft.
Fluid	Fractor coolant
Design pressure	520 psig
Design temperature	212°F
Material	Stainless steel 316L
Shell side:	Fractor coolant
Fluid	Deionized water
Design pressure	150 psig
Design temperature	200°F
Material	Carbon Steel

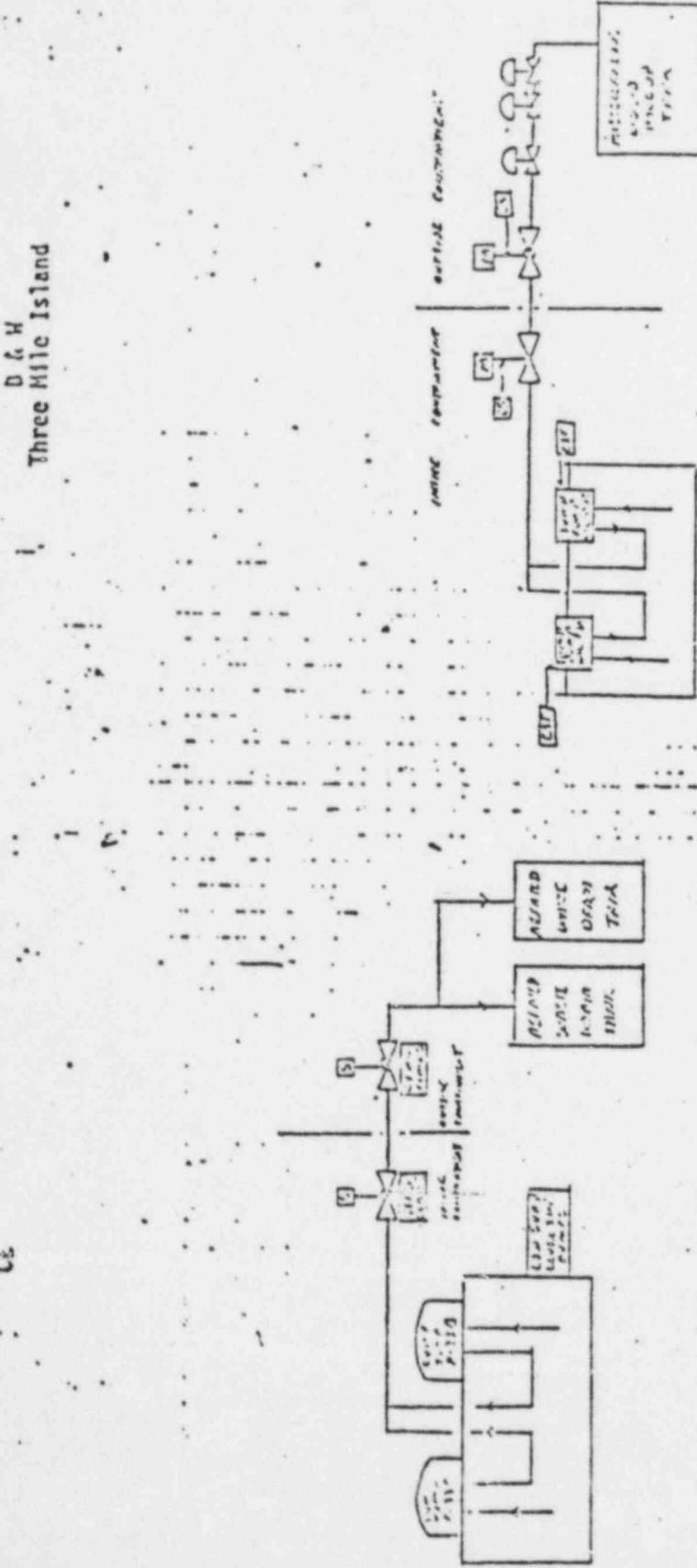
Quantity	1
Type	Deep well removal
Tube side:	Fractor coolant
Fluid	Deionized water
Design pressure	150 psig
Design temperature	200°F
Material	Carbon Steel

1240

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48

D & W
Three Mile Island



MISCELLANEOUS SYSTEM EQUIPMENT

- 1. Pneumatically Actuated, 100 gpm each
- 2. 100% level Interlock Stop Pumps
- 3. 100% Actuated (One Closed on S1A3, One on C1M), Solenoid Operated
- 4. 5000 gal each, ASME Section VIII, ASME Category I
- 5. 6000 Gal Crating Pressure
- 6. 177 ft Head Pressure
- 7. 150 ft Design Head pressure

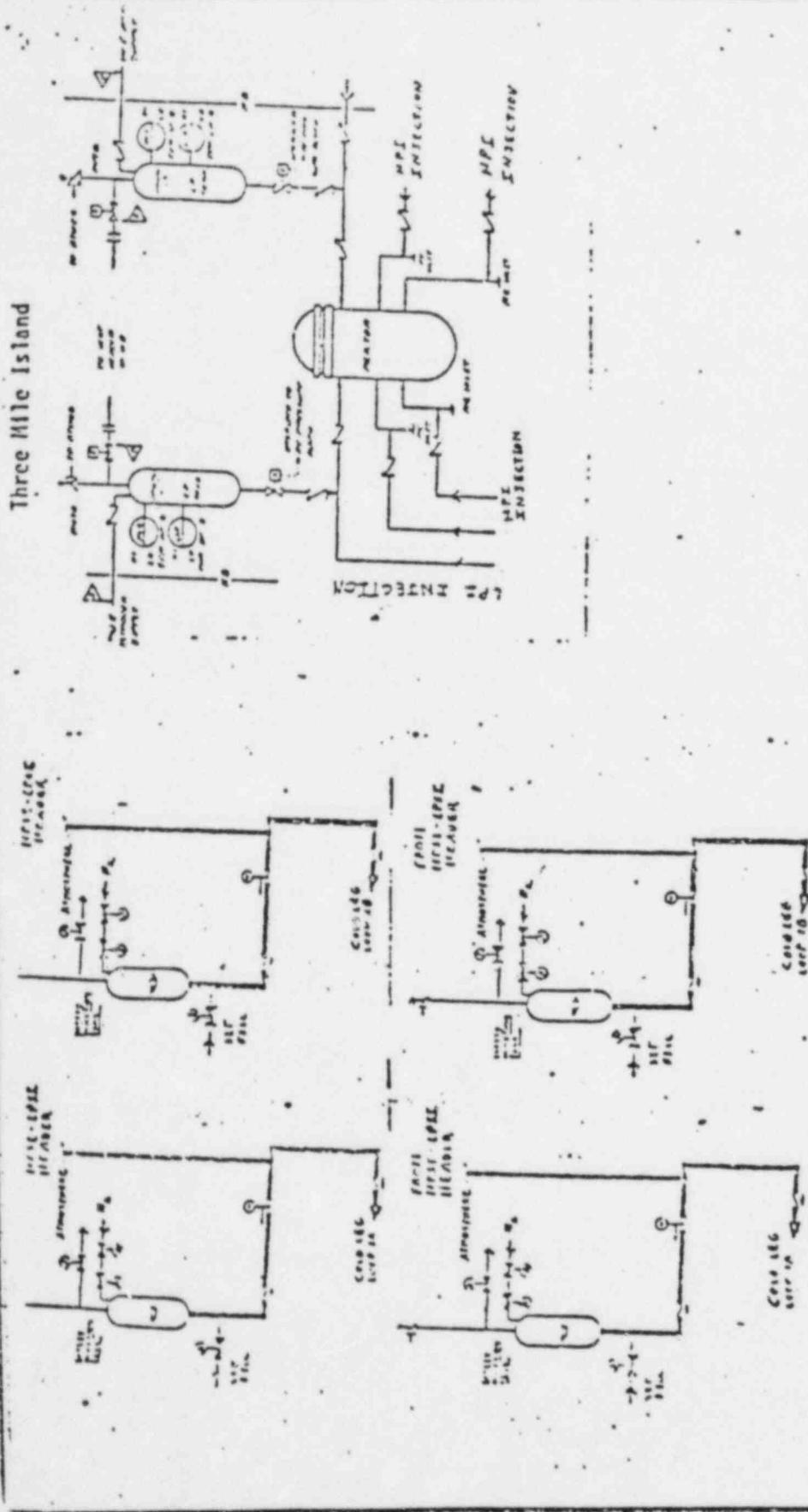
MISCELLANEOUS WASTE SYSTEM COMPONENTS

- 1. Pneumatic LSV Signal, 200 open each
- 2. Motor Operated, Receive LSV Signal
- 3. 2534 ft³ (-1814 gal.)
- 4. Storage Category I
- 5. ASME III - C Class 1
- 6. 20 ft³ Crating Protection
- 7. 150 ft Design Head pressure

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Three Mile Island



Cooling Tower Parameters

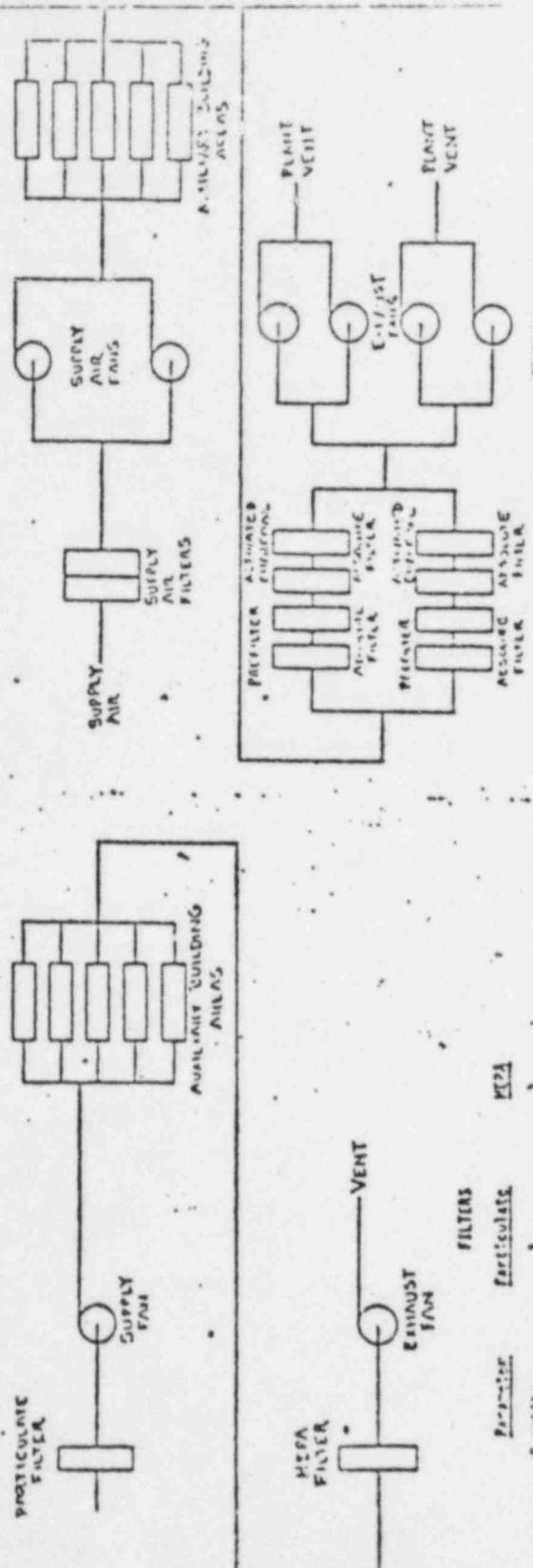
Number	4
Design pressure	250 psig
Design temperature	100 °F
Operating pressure	215 psig
Operating temperature	120 °F
Total volume	2010 ft. ³

Cooling Tower Parameters

Number	2
Design pressure	700 psig
Design temperature	300 °F
Operating pressure	620 psig
Operating temperature	110 °F
Total volume	1410 ft. ³

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Three Mile Island



Parameter	Supply Air	Prefilter	Absolute Filter	Activated Charcoal	Efficiency
Quantity	1	1	30/Asterly	92/Asterly	99.9%
Type	Automatically Advanced Rolled Media	High Efficiency Particulate Air [HEPA]	Particulate Air Charcoal	Activated Charcoal	P-1A
Size	19" x 11" x 8"	10" x 10" x 4"	34" x 24" x 4"	24" x 24" x 4"	11 1/2" P-Grid
Differential Pressure [in. W.G.]	0.16	0.16	1.2	1.0	1.2
Capacity [CFM]	22500	22500	22500	22500	22500

Part C

GENERIC RESPONSE OF AN OPERATING C-E PLANT TO
LOSS OF FEEDWATER OR A STUCK PRESSURIZER RELIEF/SAFETY VALVE

In the event of a complete loss of feedwater, the immediate response of a C-E NSSS would be a decrease in steam generator level. The loss of subcooled feedwater flow would result in a moderate reduction in steam generator heat removal capability and a slow rise in reactor coolant system (RCS) pressure and temperature. Within 15 to 40 seconds, a reactor trip signal will be produced by low steam generator level, resulting in a reactor trip and a turbine trip (for a plant with a manually initiated auxiliary feedwater system). After trip, the dump and bypass (if in the normal automatic mode) will regulate steam generator and RCS pressure and temperature to hot standby conditions and the power operated relief valve would not open.

The steam generator pressure will stabilize within a couple of minutes; decay heat will be removed through the dump and bypass. This condition could exist for 10 to 20 minutes before the heat transfer capability would start to decrease due to an excessively low steam generator level, thereby resulting in an increase in RCS temperature and pressure. If auxiliary feedwater is initiated within this time period, the power operated relief valve will not open.

For an event which does open the power operated relief or safety valve and which is followed by the unanticipated failure of a pressurizer relief or safety valve to reseat, the RCS will rapidly depressurize. If the relief valve does not reseat, the downstream isolation valve could be manually closed once the RCS pressure drops below the relief valve closing setpoint. If the valve is not, or cannot be isolated, the depressurization will continue. In this situation, the pressurizer surge tank rupture disk will fail, releasing fluid to the containment and the pressurizer bubble may be lost, resulting in liquid relief through the valve. The release of significant RCS fluid to the containment would result in a containment isolation signal.

Before the RCS pressure approaches the saturation pressure of the hot leg, a safety injection signal will occur, automatically starting the high pressure safety injection (HPSI) pumps. If the flow of the HPSI pump is sufficient to increase RCS pressure, there is no incentive for the operator to turn off these pumps to prevent overpressurization since the HPSI shutoff head is below the power operated relief valve setpoint.* If only minimum safeguards are available (i.e., one HPSI pump) due to loss of offsite power and a failure of a diesel or HPSI pump to start, the HPSI flow will be adequate to keep the core cooled. If the reactor coolant pumps are tripped, the core will be adequately cooled as long as the ECCS flow is maintained and the steam generators continue to remove decay heat. The layout of the RCS enhances core cooling because the core is essentially at the lowest elevation of the system, thereby, requiring less than 25% of the RCS inventory to keep the core covered.

R. Indleg. Jr.

*This statement does not apply to Maine Yankee which has high shutoff head pumps.

Subsequent cooldown of the RCS must be regulated within rates specified by existing procedures, by manual control of auxiliary feedwater flow, and dump valve flow. The cooldown must not be so rapid as to also cause a depressurization below the saturation pressure of the hot leg.

Depressurization must be controlled within the appropriate existing pressure-temperature guidelines by balancing of the ECCS flow with the stuck pressurizer valve flow and other flows out of the RCS, as well as the shrinkage of the RCS as it cools down; again, to assure that the RCS pressure remains above the hot leg saturation pressure.

Knobles Jr.