

EFFLUENT MONITORING REPORT

STACK EMISSIONS

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ABSTRACT

To comply with license condition 26 of license number SUA-1354, air samples were taken from five (5) stacks to determine the average and maximum concentrations ($\mu\text{Ci/cc}$) and release rates ($\mu\text{Ci/sec}$) for $\text{U}_{(n)}$, Ra-226 and Th-230, and the total quantity of uranium released (μCi).

Stack sampling was carried out by standard stack sampling techniques for air particulate sampling, employing the apparatus (Fig. 5-1) and sampling procedures shown in the Federal Register, Vol. 36, No. 47 dated December 23, 1971. (Attachment I).

Isokenetic samples were taken in the vertical section of the stacks at 25, 50, and 75 percent of the diameter, using a one way traverse. Five samples were taken from each stack with a minimum sampling time of 30 minutes per sample. Sampling time, rates and volumes are summarized in Tables I and II.

Daily grab samples were taken at each stack and composited for a one week period. The composite samples were placed in a plastic bag and sent to a commercial laboratory (EAL Corp. of Richmond, Calif.) for analysis of $\text{U}_{(n)}$, Ra-226, and Th-230. Data taken during each sampling period was recorded on standard EPA data sheets. A copy of one set of data sheets used for a single sample is attached. (Attachment II)

Methods of calculation are shown in the attached calculation data sheets, pages 1 thru 11, (Attachment III). Results of the calculations are summarized in Tables III & IV, along with a copy of the radionuclide concentrations reported by EAL Laboratories. (Attachment IV.)

Data in Table III shows that the concentrations of $\text{U}_{(nat)}$, Th-230, Ra-226 are below the MPC limits as specified in 10 CFR-20, Appendix B, Table II for all stacks.

ATTACHMENT I

SAMPLING EQUIPMENT AND PROCEDURES

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4.2 Gas volume.

$$V_{ms} = V_m \left(\frac{P_m}{P_{std}} \right) \left(\frac{T_{std}}{T_m} \right) = 17.71 \frac{^{\circ}\text{R}}{\text{in. Hg}} \left(\frac{V_m P_m}{T_m} \right) \quad \text{equation 4-2}$$

where:

V_{ms} = Dry gas volume through meter at standard conditions, cu. ft.

V_m = Dry gas volume measured by meter, cu. ft.

P_m = Barometric pressure at the dry gas meter, inches Hg.

P_{std} = Pressure at standard conditions, 29.92 inches Hg.

T_{std} = Absolute temperature at standard conditions, 530° R.

T_m = Absolute temperature at meter (°F + 460), °R.

4.3 Moisture content.

$$B_{wo} = \frac{V_{ws}}{V_{ws} + V_m} + B_{sm} = \frac{V_{ws}}{V_{ws} + V_{ms}} + (0.025) \quad \text{equation 4-3}$$

where:

B_{wo} = Proportion by volume of water vapor in the gas stream, dimensionless.

V_{ws} = Volume of water vapor collected (standard conditions), cu. ft.

V_{ms} = Dry gas volume through meter (standard conditions), cu. ft.

B_{sm} = Approximate volumetric proportion of water vapor in the gas stream leaving the impingers, 0.025.

5. References.

Air Pollution Engineering Manual, Danielson, J. A. (ed.), U.S. DHEW, PHS, National Center for Air Pollution Control, Cincinnati, Ohio, PHS Publication No. 999-AP-40, 1967.

Devorkin, Howard, et al., Air Pollution Source Testing Manual, Air Pollution Control District, Los Angeles, Calif., November 1963.

Methods for Determination of Velocity, Volume, Dust and Mist Content of Gases, Western Precipitation Division of Joy Manufacturing Co., Los Angeles, Calif., Bulletin WP-50, 1963.

METHOD 5—DETERMINATION OF PARTICULATE EMISSIONS FROM STATIONARY SOURCES

1. Principle and applicability.

1.1 Principle. Particulate matter is withdrawn isokinetically from the source and its weight is determined gravimetrically after removal of uncombined water.

1.2 Applicability. This method is applicable for the determination of particulate emissions from stationary sources only when specified by the test procedures for determining compliance with New Source Performance Standards.

2. Apparatus.

2.1 Sampling train. The design specifications of the particulate sampling train used by EPA (Figure 5-1) are described in APTD-0581. Commercial models of this train are available.

2.1.1 Nozzle—Stainless steel (316) with sharp, tapered leading edge.

2.1.2 Probe—Pyrex¹ glass with a heating system capable of maintaining a minimum gas temperature of 250° F. at the exit end during sampling to prevent condensation from occurring. When length limitations (greater than about 8 ft.) are encountered at temperatures less than 600° F., Incoloy 825², or equivalent, may be used. Probes for sampling gas streams at temperatures in excess of 600° F. must have been approved by the Administrator.

2.1.3 Pitot tube—Type S, or equivalent, attached to probe to monitor stack gas velocity.

¹ Trade name.

RULES AND REGULATIONS

2.1.4 Filter Holder—Pyrex¹ glass with heating system capable of maintaining minimum temperature of 225° F.

2.1.5 Impingers / Condenser—Four impingers connected in series with glass ball joint fittings. The first, third, and fourth impingers are of the Greenburg-Smith design, modified by replacing the tip with a 1/2-inch ID glass tube extending to one-half inch from the bottom of the flask. The second impinger is of the Greenburg-Smith design with the standard tip. A condenser may be used in place of the impingers provided that the moisture content of the stack gas can still be determined.

2.1.6 Metering system—Vacuum gauge, leak-free pump, thermometers capable of measuring temperature to within 5° F., dry gas meter with 2% accuracy, and related equipment, or equivalent, as required to maintain an isokinetic sampling rate and to determine sample volume.

2.1.7 Barometer—To measure atmospheric pressure to ±0.1 inches Hg.

2.2 Sample recovery.

2.2.1 Probe brush—At least as long as probe.

2.2.2 Glass wash bottles—Two.

2.2.3 Glass sample storage containers.

2.2.4 Graduated cylinder—250 ml.

2.3 Analysis.

2.3.1 Glass weighing dishes.

2.3.2 Desiccator.

2.3.3 Analytical balance—To measure to ±0.1 mg.

2.3.4 Trip balance—300 g. capacity, to measure to ±0.05 g.

3. Reagents.

3.1 Sampling.

3.1.1 Filters—Glass fiber, MSA 1106 BH¹, or equivalent, numbered for identification and preweighed.

3.1.2 Silica gel—Indicating type, 6-16 mesh, dried at 175° C. (350° F.) for 2 hours.

3.1.3 Water.

3.1.4 Crushed ice.

3.2 Sample recovery.

3.2.1 Acetone—Reagent grade.

3.3 Analysis.

3.3.1 Water.

IMPINGER TRAIN OPTIONAL. MAY BE REPLACED BY AN EQUIVALENT CONDENSER

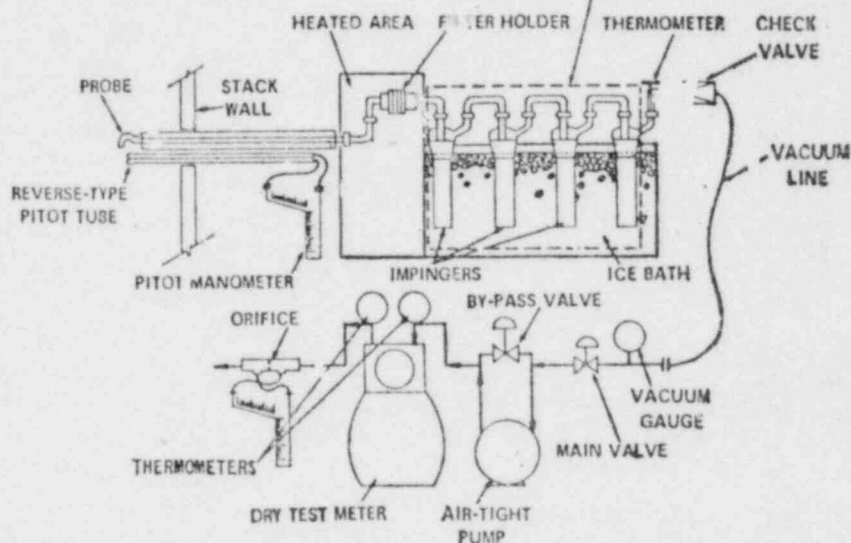


Figure 5-1. Particulate-sampling train.

3.3.2 Desiccant—Drierite¹ or heating.

4. Procedure.

4.1 Sampling.

4.1.1 After selecting the sampling site and the minimum number of sampling points, determine the stack pressure, temperature, moisture, and range of velocity head.

4.1.2 Preparation of collection train. Weigh to the nearest gram approximately 200 g. of silica gel. Label a filter of proper diameter, desiccate² for at least 24 hours and weigh to the nearest 0.5 mg. in a room where the relative humidity is less than 50%. Place 100 ml. of water in each of the first two impingers, leave the third impinger empty, and place approximately 200 g. of preweighed silica gel in the fourth impinger. Set up the train without the probe as in Figure 5-1. Leak check the sampling train at the sampling site by plugging up the inlet to the filter holder and pulling a 15 in. Hg vacuum. A leakage rate not in excess of 0.02 c.f.m. at a vacuum of 15 in. Hg is acceptable. Attach the probe and adjust the heater to provide a gas temperature of about 250° F. at the probe outlet. Turn on the filter heating system. Place crushed ice around the impingers. Add

more ice during the run to keep the temperature of the gases leaving the last impinger as low as possible and preferably at 70° F. or less. Temperatures above 70° F. may result in damage to the dry gas meter from either moisture condensation or excessive heat.

4.1.3 Particulate train operation. For each run, record the data required on the example sheet shown in Figure 5-2. Take readings at each sampling point, at least every 5 minutes, and when significant changes in stack conditions necessitate additional adjustments in flow rate. To begin sampling, position the nozzle at the first traverse point with the tip pointing directly into the gas stream. Immediately start the pump and adjust the flow to isokinetic conditions. Sample for at least 5 minutes at each traverse point; sampling time must be the same for each point. Maintain isokinetic sampling throughout the sampling period. Nomographs are available which aid in the rapid adjustment of the sampling rate without other computations. APTD-0576 details the procedure for using these nomographs. Turn off the pump at the conclusion of each run and record the final readings. Remove the probe and nozzle from the stack and handle in accordance with the sample recovery process described in section 4.2.

¹ Trade name.

² Dry using Drierite¹ at 70° F. ± 10° F.

ATTACHMENT II

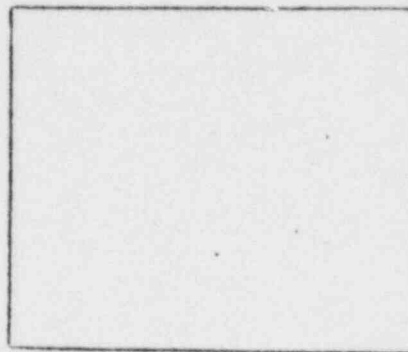
STACK SAMPLING DATA SHEETS

EPA Forms

Test No _____

Date _____

Process _____

DATA SUMMATION

Schematic of Stack

As.....	<u>3.14</u>
Ps.....	<u>25.48</u>
Barometric pressure.....	<u>25.47</u>
Cp.....	<u>.85</u>
Average square root of velocity head....	<u>.64</u>
Average pressure differential across orifice.....	<u>1.53</u>
Average dry gas meter temperature.....	<u>95°F</u>
Average stack temperature.....	<u>84</u>
Number of traverse points.....	<u>3</u>
Vm.....	<u>24.4</u>
Total particulate catch.....	_____
Meter correction factor.....	<u>.969</u>
Total beryllium catch	_____

Test No. _____

Date _____

Process _____

CALCULATIONS

- 1) Volume of water collected.

$$\begin{aligned}
 V_{wc} &= (V_{fc} - V_{ic}) \frac{p_{H_2O}}{M_{H_2O}} \frac{T_{std}}{P_{std}} R \\
 &= (0.0474 \frac{\text{cu. ft.}}{\text{m.}}) (V_{fc} - V_{ic}) \\
 &= (0.0474) (\quad)
 \end{aligned}$$

$$V_{wc} = \text{ft}^3 \text{ at } 70^\circ \text{ F and } 29.92 \text{ in. Hg.}$$

- 2) Volume of air metered.

$$\begin{aligned}
 V_{mstd} &= V_m \left(\frac{T_{std}}{T_m} \right) \left(\frac{P_{bar} + \frac{\Delta H}{13.6}}{P_{std}} \right) \\
 &= 24.4 \times .955 \times .855 \times .969
 \end{aligned}$$

.113
1.53
.969
(mcf).

= 19.3

- 3) Moisture Content.

$$B_{wo} = \frac{V_{wcstd}}{V_{mstd} + V_{wcstd}} =$$

$$\% H_2O = B_{wo} \times 100 = .025 \times 100$$

$$\% H_2O = 2.5\%$$

Test No. _____

Date _____

Process _____

$$\begin{aligned}
 4) \quad M_d &= (\% \text{CO}_2 \times \frac{44}{100}) + \\
 &\quad (\% \text{O}_2 \times \frac{32}{100}) + \\
 &\quad (\% \text{CO} \times \frac{28}{100}) + \\
 &\quad (\% \text{N}_2 \times \frac{28}{100}) \\
 &= 28.82
 \end{aligned}$$

5) Molecular weight of stack gases.

$$\begin{aligned}
 M_s &= M_d (1 - B_{wo}) + 18 (B_{wo}) \\
 M_s &= M_d (.975) + 18 (.025) \\
 M_s &= 28.55
 \end{aligned}$$

6) Velocity of exit gases.

$$V_s = K_P C_P \sqrt{\frac{T_s}{P_s M_s}} \sqrt{\Delta P} = 85.48 \times .85 \sqrt{\frac{544}{25.48 \times 28.55}} \times .64$$

.86
127

$$V_s = 40.0 \text{ fps}$$

(7) Total flow of stack gases.

$$Q_s = A_s V_s \times \frac{60}{60} = 7536 \text{ ACFM}$$

$$(Q_s)_{\text{std}} = Q_s \left(\frac{P_s}{P_{\text{std}}} \right) \left(\frac{T_{\text{std}}}{T_s} \right) (1 - B_{wo})$$

25.48
20.92
.2516

530
544
.9743

.975

$$(Q_s)_{\text{std}} = 5,901 \text{ SCFM}$$

$$V_{s \text{ std}} = \frac{5,901}{3.14 \times 60} = 31.3 \text{ Fps}$$

188.4

Test No. _____

Date _____

Process _____

8) Emissions from stack

a) Particulate

$$C_s = \frac{m_n \times 0.0154}{V_{mstd}} =$$

$$C_s = \text{gr/scf}$$

$$pmr = \frac{(m_n) (Q)_s \text{ std } (60)}{V_{mstd} (454,000)} =$$

b) Beryllium

$$R = \frac{Wt (V_s) \text{ std } As \times 86,400 \text{ secs/day}}{V_{mstd} 10^6 \text{ } \gamma/g}$$

$$R = \text{g/day}$$

$$9) \text{ Percent Isokinetic } = \frac{V_{mstd}}{A_n @ V_s \text{ std}} = \frac{19.3}{.0003408 \times 30 \times 31.3 \times 60} \times 100 = 19.2$$

10) Summary of emission data:

a) Regulation 123.13 "Particulate"

Allowable Emissions
0.02 grains per SFF

Measured Emissions

Regulation 61.32 "Beryllium"

10 grams/day
0.01 γ/M^3 monthly average

100.5%

ATTACHMENT III
CALCULATIONS

Stack Sampling Data

Average Concentration and Release Rates for Uranium

License Condition 26A

1. Average and maximum uranium concentration ($\mu\text{Ci/cc}$) measured at the uranium recovery operations stack.

$$\begin{aligned}\mu\text{Ci/sample} &= 4.4 \pm 0.2 \text{ pCi/sample} \times 10^{-6} \mu\text{Ci/pCi} \\ &= 4.4 \pm 0.2 \times 10^{-6} \mu\text{Ci/sample}\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/ft.}^3 &= 4.4 \times 10^{-6} \mu\text{Ci/sample} \div 131.82 \text{ ft.}^3/\text{sample} \\ &= 0.0335 \times 10^{-6} \mu\text{Ci/ft.}^3\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/M}^3 &= 0.0335 \times 10^{-6} \mu\text{Ci/ft.}^3 \times 35.3 \text{ ft.}^3/\text{M}^3 \\ &= 1.183 \times 10^{-6} \mu\text{Ci/M}^3\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/cc} &= 1.183 \times 10^{-6} \mu\text{Ci/M}^3 \times \text{M}^3/10^6 \text{ cc} \\ &= 1.183 \times 10^{-12} \mu\text{Ci/cc}\end{aligned}$$

License Condition 26B

a. Uranium Stack

1. Average Uranium Release Rate ($\mu\text{Ci/sec}$)

$$\begin{aligned}\text{Average velocity of exit gases} &= 30.82 \text{ fps} \\ \text{Area of stack} &= 3.14 \text{ ft}^2\end{aligned}$$

$$\begin{aligned}\text{ft}^3/\text{sec} &= 30.82 \text{ fps} \times 3.14 \text{ ft}^2 \\ &= 96.79 \text{ ft}^3/\text{sec}\end{aligned}$$

$$\begin{aligned}\text{cc/sec} &= 96.79 \text{ ft}^3/\text{sec} \times 2.832 \times 10^4 \text{ cc/ft}^3 \\ &= 274 \times 10^4 \text{ cc/sec}\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/sec} &= 1.183 \times 10^{-12} \mu\text{Ci/cc} \times 274 \times 10^4 \text{ cc/sec} \\ &= 324.14 \times 10^{-8} \\ &= 3.24 \times 10^{-6} \mu\text{Ci/sec.}\end{aligned}$$

2. Total Quantity of Uranium Released (μCi)

$$\begin{aligned}\mu\text{Ci} &= 3.24 \times 10^{-6} \mu\text{Ci/sec} \times 86,400 \text{ sec/day} \times 140 \text{ days} \\ &= 39.19 \mu\text{Ci}\end{aligned}$$

b. Old Leach Stack

1. Average uranium release rate ($\mu\text{Ci/sec}$)

$$\text{Average velocity of exit gases} = 5.4 \text{ fps}$$

$$\text{Area of stack} = 3.14 \text{ ft}^2$$

$$\text{Sample volume} = 135.5 \text{ ft}^3$$

$$\begin{aligned} \mu\text{Ci/sample} &= 0.4 \pm \text{pCi/sample} \times 10^{-6} \mu\text{Ci/pCi} \\ &= 0.4 \times 10^{-6} \mu\text{Ci/sample} \end{aligned}$$

$$\begin{aligned} \mu\text{Ci/ft}^3 &= 0.4 \times 10^{-6} \mu\text{Ci/sample} \div 135.5 \text{ ft}^3/\text{sample} \\ &= .00295 \times 10^{-6} \mu\text{Ci/ft}^3 \end{aligned}$$

$$\begin{aligned} \mu\text{Ci/M}^3 &= .00295 \times 10^{-6} \mu\text{Ci/ft}^3 \times 35.3 \text{ ft}^3/\text{M}^3 \\ &= 0.1041 \times 10^{-6} \end{aligned}$$

$$\begin{aligned} \mu\text{Ci/cc} &= 0.1041 \times 10^{-6} \mu\text{Ci/M}^3 \times \frac{\text{M}^3}{10^{-6} \text{ cc}} \\ &= 0.1041 \times 10^{-12} \mu\text{Ci/cc} \end{aligned}$$

$$\begin{aligned} \text{ft}^3/\text{sec} &= 5.4 \text{ fps} \times 3.14 \text{ ft}^2 \\ &= 16.96 \text{ ft}^3/\text{sec.} \end{aligned}$$

$$\begin{aligned} \text{cc/sec} &= 16.96 \text{ ft}^3/\text{sec} \times 2.832 \times 10^4 \text{ cc/ft}^3 \\ &= 48.03 \times 10^4 \text{ cc/sec.} \end{aligned}$$

$$\begin{aligned} \mu\text{Ci/sec} &= 0.1041 \times 10^{-12} \mu\text{Ci/cc} \times 48.03 \times 10^4 \text{ cc/sec} \\ &= 4.995 \times 10^{-8} \mu\text{Ci/sec.} \end{aligned}$$

2. Total quantity of uranium released (μCi)

$$\begin{aligned} \mu\text{Ci} &= 4.995 \times 10^{-8} \mu\text{Ci/sec} \times 86,400 \text{ sec/day} \times 140 \text{ days} \\ &= 60,419,520 \times 10^{-8} \\ &= 0.6 \mu\text{Ci} \end{aligned}$$

C. New Leach Stack

1. Average uranium release rate ($\mu\text{Ci/sec}$)

$$\begin{aligned}\text{Average velocity of exit gases} &= 13.44 \text{ fps} \\ \text{Area of stack} &= 3.14 \text{ ft}^2 \\ \text{Sample volume} &= 113.3 \text{ ft}^3\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/sample} &= 0.4 \pm 0.1 \text{ pCi/sample} \times 10^{-6} \mu\text{Ci/pCi} \\ &= 0.4 \pm 0.1 \times 10^{-6} \mu\text{Ci/sample} \\ \mu\text{Ci/ft}^3 &= 0.4 \times 10^{-6} \mu\text{Ci/sample} \div 113.3 \text{ ft}^3/\text{sample} \\ &= 0.0035 \times 10^{-6} \mu\text{Ci/ft}^3\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/M}^3 &= 0.0035 \times 10^{-6} \mu\text{Ci/ft}^3 \times 35.3 \text{ ft}^3/\text{M}^3 \\ &= 0.1246 \times 10^{-6} \mu\text{Ci/M}^3\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/cc} &= 0.1246 \times 10^{-6} \mu\text{Ci/M}^3 \times \text{M}^3/10^6 \text{ cc} \\ &= 0.1246 \times 10^{-12} \mu\text{Ci/cc}\end{aligned}$$

$$\begin{aligned}\text{ft}^3/\text{sec} &= 13.44 \text{ fps} \times 3.14 \text{ ft}^2 \\ &= 42.20 \text{ ft}^3/\text{sec}\end{aligned}$$

$$\begin{aligned}\text{cc/sec} &= 42.20 \text{ ft}^3/\text{sec} \times 2.832 \times 10^4 \text{ cc/ft}^3 \\ &= 119.01 \times 10^4 \text{ cc/sec}\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/sec} &= 0.1246 \times 10^{-12} \mu\text{Ci/cc} \times 119.01 \times 10^4 \text{ cc/sec} \\ &= 14.83 \times 10^{-8} \mu\text{Ci/sec}\end{aligned}$$

2. Total quantity of uranium released (μCi)

$$\begin{aligned}\mu\text{Ci} &= 14.83 \times 10^{-8} \mu\text{Ci/sec} \times 86,400 \text{ sec/day} \times 140 \text{ days} \\ &= 179,383,680 \times 10^{-8} \mu\text{Ci} \\ &= 1.79 \mu\text{Ci}\end{aligned}$$

D. Be-Hydrolysis Drumming Stack

1. Average Uranium release rate ($\mu\text{Ci/sec}$)

$$\begin{aligned}\text{Average velocity of exit gases} &= 7.3 \text{ fps} \\ \text{Area of stack} &= 3.14 \text{ ft}^2 \\ \text{Sample Volume} &= 119.8 \text{ ft}^3\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/sample} &= 0.5 \pm \text{pci/sample} \times 10^{-6} \mu\text{Ci/pCi} \\ &= 0.5 \pm 0.1 \times 10^{-6} \mu\text{Ci/sample}\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/ft}^3 &= 0.5 \times 10^{-6} \mu\text{Ci/sample} \div 119.8 \text{ ft}^3/\text{sample} \\ &= .0042 \times 10^{-6} \mu\text{Ci/ft}^3\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/M}^3 &= 0.0042 \times 10^{-6} \mu\text{Ci/ft}^3 \times 35.3 \text{ ft}^3/\text{M}^3 \\ &= 0.1483 \times 10^{-6} \mu\text{Ci/M}^3\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/cc} &= 0.1483 \times 10^{-6} \mu\text{Ci/M}^3 \times \text{M}^3/10^6 \text{ cc} \\ &= 0.1483 \times 10^{-12} \mu\text{Ci/cc}\end{aligned}$$

$$\begin{aligned}\text{ft}^3/\text{sec} &= 7.3 \text{ fps} \times 3.14 \text{ ft}^2 \\ &= 22.92 \text{ ft}^3/\text{sec}.\end{aligned}$$

$$\begin{aligned}\text{cc/sec} &= 22.92 \text{ ft}^3/\text{sec} \times 2.832 \times 10^4 \text{ cc/ft}^3 \\ &= 64.92 \times 10^4 \text{ cc/sec}\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/sec} &= 0.1483 \times 10^{-12} \mu\text{Ci/cc} \times 64.92 \times 10^4 \text{ cc/sec} \\ &= 9.62 \times 10^{-8} \mu\text{Ci/sec}\end{aligned}$$

2. Total Quantity of Uranium released (μCi)

$$\begin{aligned}\mu\text{Ci} &= 9.62 \times 10^{-8} \mu\text{Ci/sec} \times 86,400 \text{ sec/day} \times 140 \text{ days} \\ &= 116,363,520 \times 10^{-8} \mu\text{Ci} \\ &= 1.16 \mu\text{Ci}\end{aligned}$$

E. Be-Hydrolysis Scrubber Stack

1. Average Uranium release rate ($\mu\text{Ci/sec}$)

$$\begin{aligned}\text{Average velocity of exit gases} &= 3.6 \text{ fps} \\ \text{Area of stack} &= 1.766 \text{ ft}^2 \\ \text{Sample volume} &= 81 \text{ ft}^3\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/sample} &= 2.2 \pm 0.2 \text{ pCi/sample} \times 10^{-6} \mu\text{Ci/pCi} \\ &= 2.2 \pm 0.2 \times 10^{-6} \mu\text{Ci/sample}\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/ft}^3 &= 2.2 \times 10^{-6} \mu\text{Ci/sample} \div 81 \text{ ft}^3/\text{sample} \\ &= .0272 \times 10^{-6} \mu\text{Ci/ft}^3\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/M}^3 &= .0272 \times 10^{-6} \mu\text{Ci/ft}^3 \times 35.3 \text{ ft}^3/\text{M}^3 \\ &= 0.960 \times 10^{-6} \mu\text{Ci/M}^3\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/cc} &= 0.960 \times 10^{-6} \mu\text{Ci/M}^3 \times \text{M}^3/10^6 \text{ cc} \\ &= 0.960 \times 10^{-12} \mu\text{Ci/cc}\end{aligned}$$

$$\begin{aligned}\text{ft}^3/\text{sec} &= 3.6 \text{ fps} \times 1.766 \text{ ft}^2 \\ &= 6.36 \text{ ft}^3/\text{sec}\end{aligned}$$

$$\begin{aligned}\text{cc/sec} &= 6.36 \text{ ft}^3/\text{sec} \times 2.832 \times 10^4 \text{ cc/ft}^3 \\ &= 18.01 \times 10^4 \text{ cc/sec}\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/sec} &= 0.960 \times 10^{-12} \mu\text{Ci/cc} \times 18.01 \times 10^4 \text{ cc/sec} \\ &= 17.29 \times 10^{-8} \mu\text{Ci/sec}\end{aligned}$$

2. Total Quantity of Uranium Released (μCi)

$$\begin{aligned}\mu\text{Ci} &= 17.29 \times 10^{-8} \mu\text{Ci/sec} \times 86,400 \frac{\text{sec.}}{\text{day}} \times 140 \text{ days} \\ &= 209,139,840 \times 10^{-8} \mu\text{Ci} \\ &= 2.09 \mu\text{Ci}\end{aligned}$$

Stack Sampling Data
Average Concentration and Release Rates for Ra-226

Pg. 6.0

License Condition 26-C

A. Uranium Stack

1. Average Concentration for Radium 226 ($\mu\text{Ci/cc}$)

$$\begin{aligned}\mu\text{Ci/sample} &= 0.29 \pm 0.08 \text{ pCi/sample} \times 10^{-6} \mu\text{Ci/pCi} \\ &= 0.29 \pm 0.08 \times 10^{-6} \mu\text{Ci/sample}\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/ft}^3 &= 0.29 \times 10^{-6} \mu\text{Ci/sample} \div 131.82 \text{ ft}^3/\text{sample} \\ &= 0.0022 \times 10^{-6} \mu\text{Ci/ft}^3\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/M}^3 &= 0.0022 \times 10^{-6} \mu\text{Ci.ft}^3 \times 35.3 \text{ ft}^3/\text{M}^3 \\ &= 0.0777 \times 10^{-6} \mu\text{Ci/M}^3\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/cc} &= 0.0777 \times 10^{-6} \mu\text{Ci/M}^3 \times \text{M}^3/10^6 \text{ cc} \\ &= 0.0777 \times 10^{-12} \mu\text{Ci/cc}\end{aligned}$$

2. Release rates for Radium 226 ($\mu\text{Ci/sec}$)

$$\begin{aligned}\text{ft}^3/\text{sec} &= 30.82 \text{ fps} \times 3.14 \text{ ft}^2 \\ &= 96.79 \text{ ft}^3/\text{sec}\end{aligned}$$

$$\begin{aligned}\text{cc/sec} &= 96.79 \text{ ft}^3/\text{sec} \times 2.832 \times 10^4 \text{ cc/ft}^3 \\ &= 274 \times 10^4 \text{ cc/sec}\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/sec} &= 0.0777 \times 10^{-12} \mu\text{Ci/cc} \times 274 \times 10^4 \text{ cc/sec} \\ &= 21.29 \times 10^{-8} \mu\text{Ci/sec} \\ &= .213 \times 10^{-6} \mu\text{Ci/sec}\end{aligned}$$

B. Old Leach Stack

1. Average Concentration for Ra-226 ($\mu\text{Ci/cc}$)

$$\begin{aligned}\mu\text{Ci/sample} &= 0.11 \pm 0.08 \text{ pCi/sample} \times 10^{-6} \mu\text{Ci/pCi} \\ &= 0.11 \pm 0.08 \times 10^{-6} \mu\text{Ci/sample}\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/ft}^3 &= 0.11 \times 10^{-6} \mu\text{Ci/sample} \div 135.5 \text{ ft}^3/\text{sample} \\ &= 0.0008 \times 10^{-6} \mu\text{Ci/ft}^3\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/M}^3 &= 0.0008 \times 10^{-6} \mu\text{Ci/ft}^3 \times 35.3 \text{ ft}^3/\text{M}^3 \\ &= 0.0287 \times 10^{-6} \mu\text{Ci/M}^3\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/cc} &= 0.0287 \times 10^{-6} \mu\text{Ci/M}^3 \times \frac{\text{M}^3}{10^6 \text{ cc}} \\ &= 0.0287 \times 10^{-12} \mu\text{Ci/cc}\end{aligned}$$

2. Release Rates for Ra-226 ($\mu\text{Ci/sec}$)

$$\begin{aligned}\text{ft}^3/\text{sec} &= 5.4 \text{ fps} \times 3.14 \text{ ft}^2 \\ &= 16.96 \text{ ft}^3/\text{sec}\end{aligned}$$

$$\begin{aligned}\text{cc/sec} &= 16.96 \text{ ft}^3/\text{sec} \times 2.832 \times 10^4 \text{ cc/ft}^3 \\ &= 48.03 \times 10^4 \text{ cc/sec}\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/sec} &= 0.0287 \times 10^{-12} \mu\text{Ci/cc} \times 48.03 \times 10^4 \text{ cc/sec} \\ &= 1.376 \times 10^{-8} \mu\text{Ci/sec} \\ &= .0138 \times 10^{-6} \mu\text{Ci/sec}\end{aligned}$$

C. New Leach Stack

1. Average Concentration for R₂-226 ($\mu\text{Ci/cc}$)

$$\begin{aligned}\mu\text{Ci/sample} &= 0.14 \pm 0.08 \text{ pCi/sample} \times 10^{-6} \mu\text{Ci/pCi} \\ &= 0.14 \pm 0.08 \times 10^{-6} \mu\text{Ci/sample}\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/ft}^3 &= 0.14 \times 10^{-6} \mu\text{Ci/sample} \div 113.3 \text{ ft}^3/\text{sample} \\ &= 0.00123 \times 10^{-6} \mu\text{Ci/ft}^3\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/M}^3 &= 0.00123 \times 10^{-6} \mu\text{Ci/ft}^3 \times 35.3 \text{ ft}^3/\text{M}^3 \\ &= 0.0434 \times 10^{-6} \mu\text{Ci/M}^3\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/cc} &= 0.0434 \times 10^{-6} \mu\text{Ci/M}^3 \times \text{M}^3/10^6 \text{ cc} \\ &= 0.0434 \times 10^{-12} \mu\text{Ci/cc}\end{aligned}$$

2. Release Rate for Ra-226 ($\mu\text{Ci/sec}$)

$$\begin{aligned}\text{ft}^3/\text{sec} &= 13.44 \text{ fps} \times 3.14 \text{ ft}^2 \\ &= 42.20 \text{ ft}^3/\text{sec}\end{aligned}$$

$$\begin{aligned}\text{cc/sec} &= 42.20 \text{ ft}^3/\text{sec} \times 2.832 \times 10^4 \text{ cc/ft}^3 \\ &= 119.01 \times 10^4 \text{ cc/sec}\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/sec} &= 0.0434 \times 10^{-12} \mu\text{Ci/cc} \times 119.01 \times 10^4 \text{ cc/sec} \\ &= 5.165 \times 10^{-8} \mu\text{Ci/sec}\end{aligned}$$

D. Beryllium Hydrolysis Drumming Stack

1. Average concentration for Ra-226 ($\mu\text{Ci/cc}$)

$$\begin{aligned}\mu\text{Ci/sample} &= 0.13 \pm 0.08 \text{ pCi/sample} \times 10^{-6} \mu\text{Ci/pCi} \\ &= 0.13 \pm 0.08 \times 10^{-6} \mu\text{Ci/sample}\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/ft}^3 &= 0.13 \times 10^{-6} \mu\text{Ci/sample} \div 119.8 \text{ ft}^3/\text{sample} \\ &= 0.0011 \times 10^{-6} \mu\text{Ci/ft}^3\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/M}^3 &= 0.0011 \times 10^{-6} \mu\text{Ci/ft}^3 \times 35.3 \text{ ft}^3/\text{M}^3 \\ &= 0.0388 \times 10^{-6} \mu\text{Ci/M}^3\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/cc} &= 0.0388 \times 10^{-6} \mu\text{Ci/M}^3 \times \text{M}^3/10^6 \text{ cc} \\ &= 0.0388 \times 10^{-12} \mu\text{Ci/cc}\end{aligned}$$

2. Release Rate for Ra-226 ($\mu\text{Ci/sec}$)

$$\begin{aligned}\text{ft}^3/\text{sec} &= 7.3 \text{ fps} \times 3.14 \text{ ft}^2 \\ &= 22.92 \text{ ft}^3/\text{sec}\end{aligned}$$

$$\begin{aligned}\text{cc/sec} &= 22.92 \text{ ft}^3/\text{sec} \times 2.832 \times 10^4 \text{ cc/ft}^3 \\ &= 64.92 \times 10^4 \text{ cc/sec}\end{aligned}$$

$$\begin{aligned}\mu\text{Ci/sec} &= 0.0388 \times 10^{-12} \mu\text{Ci/cc} \times 64.92 \times 10^4 \text{ cc/sec} \\ &= 2.52 \times 10^{-8} \mu\text{Ci/sec}\end{aligned}$$

E. Beryllium Hydrolysis Scrubber Stack

1. Average Concentration for Ra-226 ($\mu\text{Ci/cc}$) = 0
2. Release rate for Ra-226 ($\mu\text{Ci/sec}$) = 0

Analysis report shows Ra-226 = 0 ± 0.09 pCi/sample

Stack Sampling Data

Average Concentration and Release Rate for Thorium - 230

License Condition 26-C

The average concentration and release rates for thorium-230 are below limits of detection as shown by Table III and by the analytical report (Attachment IV).

ATTACHMENT IV

CHEMICAL ANALYSIS OF STACK SAMPLES

ATTACHMENT IV RESULTS

Sample Number	Analysis	Results pCi/sample $\pm 2 \sigma$
D-9343 Uranium Stack	^{226}Ra	0.29 ± 0.08
	^{230}Th	0 ± 0.2
	^{238}U	4.4 ± 0.2
D-9344 Old Leach Stack	^{226}Ra	0.11 ± 0.08
	^{230}Th	0 ± 0.3
	^{238}U	0.4 ± 0.1
D-9345 New Leach Stack	^{226}Ra	0.14 ± 0.08
	^{230}Th	0 ± 0.2
	^{238}U	0.4 ± 0.1
D-9346 Be-Hyd Drumming	^{226}Ra	0.13 ± 0.08
	^{230}Th	0 ± 0.2
	^{238}U	0.5 ± 0.1
D-9347 Be-Hyd Scrubber	^{226}Ra	0 ± 0.09
	^{230}Th	0 ± 0.3
	^{238}U	2.2 ± 0.2

TABLE I
Stack Sampling Data
1st Half 1981

Date	Sample Volume		Sample		Stack Velocity		% Iso-Kenetic	Stack Temp. °F
	Vm CF	Vm. Std. SCF	Time (Min.)	% H ₂ O	Vs. fps	Vs. Std. fps		
A) Uranium Stack								
6-1-81	24.40	19.3	30	2.5	40.0	31.3	100.5	84
6-2-81	21.15	16.9	30	2.2	38.1	31.1	88.7	79
6-3-81	23.80	18.5	30	2.4	34.1	28.1	107.6	75
6-4-81	47.20	38.7	60	2.0	38.7	31.9	99.0	79
6-5-81	48.80	38.4	60	2.4	38.8	31.7	98.7	82
B) Old Leach Stack								
6-8-81	35.4	27.7	60	25.0	9.7	5.4	104.5	149
6-9-81	38.7	30.7	60	22.0	10.3	6.0	104.0	144
6-9-81	38.9	30.5	60	22.0	10.3	6.0	103.4	144
6-10-81	30.5	23.9	60	35.0	10.8	5.1	95.6	167
6-10-81	28.4	22.7	60	26.0	8.4	4.6	101.2	154
C) New Leach Stack								
6-3-81	24.1	19.7	30	41.0	32.0	13.5	105.9	171
6-4-81	45.0	36.2	60	46.0	31.1	12.0	109.4	176
6-5-81	24.7	19.3	30	41.0	32.7	13.9	100.5	171
6-8-81	25.0	19.5	30	41.0	33.0	13.9	101.6	171
6-9-81	23.7	18.6	30	41.0	33.0	13.9	96.9	171
D) Be-Hydrolysis Drumming								
6-1-81	23.5	18.7	30	5.0	10.1	7.8	97.9	93
6-2-81	10.7	8.5	30	5.0	7.8	6.0	103.7	93
6-3-81	19.8	15.6	30	5.0	8.3	6.4	99.4	92
6-5-81	50.3	39.3	60	6.0	10.9	8.3	96.6	97
6-6-81	48.3	37.7	60	5.0	10.1	7.8	98.4	93
E) Be-Hydrolysis Scrubber								
6-3-81	14.2	11.5	30	30.0	8.6	4.4	106.5	158
6-4-81	22.6	17.7	60	32.0	7.1	3.5	103.5	160
6-5-81	22.9	17.8	60	31.0	7.0	3.5	103.5	158
6-6-81	22.7	17.5	60	36.0	7.2	3.3	108.0	165
6-8-81	21.0	16.5	60	27.0	6.3	3.4	98.8	156

TABLE II

Stack Sampling Data

Sample No.	Stack Identification	Date Collected	Sample Volume SCF	Sample Time (min)	Stack Vel. FPS (Avg.)	Stack Area ft ²	Stack Temp (Avg.)	Stack %H ₂ O (Avg.)
D-9343	Uranium Stack	6-1 6-5	131.8	210	30.82	3.14	79.8	2.3
D-9344	Old Leach Stack	6-8 6-10	135.5	300	5.4	3.14	151.6	26.0
D-9345	New Leach Stack	6-3 6-9	113.3	180	13.4	3.14	172.0	42.0
D-9346	Be-Hyd. Drumming	6-1 6-6	119.8	210	7.3	3.14	93.6	5.2
D-9347	Be-Hyd. Scrubber	6-3 6-8	81.0	270	3.6	1.77	159.4	31.2

TABLE III

Stack Sampling Data

Sample No.	Stack Ident.	Radionuclide Conc.			Avg. & Max. U-Conc. (μ Ci/cc) 1×10^{-12}	Avg. U-Rel. Rate (μ Ci/sec) 1×10^{-6}	Quant. U-Rel. (μ Ci)	Avg. Conc.		Avg. Release	
		U-238	Ra-226 pCi/sample	Th-230				Ra-226 (μ Ci/cc) 1×10^{-12}	Th-230	Ra-226 (μ Ci/sec) 10^{-6}	Th-230
D-9343	U Stack	4.4 $\pm$ 0.2	0.29 $\pm$.08	0 $\pm$ 0.2	1.183	3.24	39.19	0.0888	0	0.213	0
D-9344	Old Leach	0.4 $\pm$ 0.1	0.11 $\pm$.08	0 $\pm$ 0.3	0.1041	0.0499	0.6	0.0287	0	0.0138	0
D-9345	New Leach	0.4 $\pm$ 0.1	0.14 $\pm$.08	0 $\pm$ 0.2	0.1246	0.1483	1.79	0.0434	0	.0517	0
D-9346	Be-Hyd. Dr.	0.5 $\pm$	0.13 $\pm$.08	0 $\pm$ 0.2	0.1483	0.0962	1.16	0.0388	0	0.0252	0
D-9347	Be-Hyd. Scr.	2.2 $\pm$ 0.2	0 $\pm$.09	0 $\pm$ 0.3	0.9600	0.1729	2.09	0	0	0	0
Total							44.83				
MPC ^a					5.0 $\times 10^{-12}$			2.0 $\times 10^{-12}$	3 $\times 10^{-13}$		
LLD ^b					5.0 $\times 10^{-13}$			2.0 $\times 10^{-13}$	3 $\times 10^{-14}$		

a As stated in Table II, appendix B, of 10CFR-20

b As stated in Regulatory Guide 4.14

TABLE IV

Stack Sampling Data

Stack I.D.	Dates Collected	U(nat)	Radionuclids Conc. μ Ci/M ³		Effluent Flow Rate Ft/sec.
			Th-230	Ra-226	
U- Stack	6-1 to 6.5	1.183	0.000	0.0777	30.82
Old Leach	6-8 to 6-10	0.1041	0.000	0.0287	5.40
New Leach	6-3 to 6.9	0.1246	0.000	0.0434	13.44
Be-Hyd. Drum	6.1 to 6.6	0.1483	0.000	0.0388	7.3
Be-Hyd. Scrub	6.3 to 6-8	0.9600	0.000	0.000	3.6