



International Agreement Report

Assessment of RELAP5/MOD2, Cycle 36.04 Against FIX-II Split Break Experiment No. 3051

Prepared by
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**Office of Nuclear Regulatory Research
U.S. Nuclear Regulatory Commission
Washington, DC 20555**

October 1989

Prepared as part of
The Agreement on Research Participation and Technical Exchange
under the International Thermal-Hydraulic Code Assessment
and Application Program (ICAP)

Published by
U.S. Nuclear Regulatory Commission

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NUREG/IA-0029



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1986-09-17

SKI Project 85026, 13.3-917/84

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Swedish Nuclear Power Inspectorate

ICAP

Assessment of RELAP5/MOD2, Cycle 36.04 Against
FIX-II Split Break Experiment No. 3051

ABSTRACT

The FIX-II split break experiment No. 3051 has been analyzed using the RELAP5/MOD2 code. The code version used, Cycle 36.04, is the frozen version of the code.

Three calculations were carried out to study the sensitivity of various parameters to the change of break discharge and passive heat structures. The differences between the calculations and the experiment have been quantified over intervals in real time for a number of variables available from the measurements during the experiment.

Approved by



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1 INTRODUCTION

There is a growing interest in modifying existing rules for reactor licensing and safety thermal-hydraulic calculation away from those stated in Appendix K (Ref 1) towards procedures based on best estimate types of calculations. Although Appendix K furnishes a set of skillfully and simply phrased rules, its present conservatism on safety is regarded as being in growing contradiction to the increasing knowledge gained from experimental programs. The many advanced best estimate thermal-hydraulic reactor codes in existence today also demonstrate this.

When the simply formulated older calculation rules are replaced by best estimate type calculation procedures another measure of reliability has to be established to ensure conservatism. Plans for conducting code assessments for the purpose of determining the accuracy and the validity of advanced LWR system codes were proposed some years ago (Ref 2). Today the International Code Assessment Program (ICAP) with this goal is being carried out under the auspices of the USNRC (Ref 3).

These calculations are presented as a Swedish contribution to the ICAP. The contribution is funded by the Swedish Nuclear Power Inspectorate.

In the present study the RELAP5/MOD2 version 36.04 is assessed against LOCA experiment No. 3051 carried out in the FIX-II test facility at Studsvik. The experiment is one from the second test series.

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Test No. 3051 is a split break simulation and had the smallest break area of all the FIX-II tests, see Table 1. The break area was 10 per cent of the scaled down area of a recirculation line in the reactor.

A description of the test facility and this particular test is provided in Chapter 2. A description of the input model is given in Chapter 3. The base case and sensitivity calculations are discussed in Chapters 4 and 5. Run statistics are given in Chapter 6. General conclusions are drawn in Chapter 7.

Appendix A contains the complete input lists. The data comparison plots are included in Appendix B. Results of the statistical analyses of differences between experiment and predictions for discrete time intervals are included in Appendix C. Finally Appendix D describes the data package on magnetic tape, prepared for use in the ICAP evaluation work.

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2 FACILITY AND TEST DESCRIPTION

The FIX-II integral test facility was completed at the end of 1981. It has been run by Studsvik Energiteknik AB under contract with the Swedish Nuclear Power Inspectorate. The experimental program comprises investigations of the fuel-to-coolant heat transfer. Various blowdown and pump trip situations conceivable in Swedish BWR's are simulated.

2.1 Test facility

The test facility is shown in Figure 1. The volume scaling is 1:777 of the Oskarshamn-II reactor, which is of the ASEA-ATOM external recirculation pump design. An exhaustive description of the FIX-II test facility may be obtained from Ref (4), which also provides additional references where various problems pertaining to the construction period are discussed. Therefore, only some fundamental aspects of the facility will be presented here.

The core model involves a full length rod bundle, which in the geometry is closely related to a fuel element of the ASEA-ATOM design and which is electrically heated by DC. Here, however, there are only 6 x 6 rod simulators instead of the 8 x 8 rods in a fuel element. Figures 2 and 3a show details from the core simulator design. As seen, filler bodies are placed between the square-section fuel channel and the circular-section pressure vessel to reduce the water-filled volume, which otherwise may influence the test by the leakage of steam to the upper plenum during depressurization. The water surrounding the fillers is externally recirculated and cooled by 200 to 250 kW.

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The upper part of the pressure vessel, Figure 3b, holds the steam separator and the steam condenser volume with its three sprinklers. During steady state power operation the steam outlet is closed. The turbine power is modelled by the partial circulation of water from the downcomer through an external 6 MW cooler with feedback to the sprinklers of the steam condenser and to the upper part of the downcomer. The flow rate in the two branches with cooled water is adjusted to control the pressure and the inlet subcooling. The remaining downcomer flow, representing the recirculation coolant flow in the reference reactor, splits at the lower downcomer end into two loops. One loop represents three of the intact recirculation lines of the reference reactor, while the other loop, representing a fourth recirculation line, incorporates the break devices. Both loops have its own recirculation pump. The intact loop pump speed is controlled according to a predetermined speed history.

The FIX-II has, as part of the core model, an external bypass simulator, Figure 30, through which about 12 % of the recirculation mass flow is diverted through a control valve. This bypass is heated separately to represent the channel wall heat transfer. At the lower end of the bypass there is a stagnant water volume to simulate the reference reactor space for the control rod guide tubes.

Since the FIX-II facility has been designed for blowdown experiments only, no emergency core cooling equipment is installed.

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The data collection system is constructed around a signal processor controlling 192 measurement channels. The selection of measurements is made in a signal exchange terminal. A multipurpose minicomputer transfers the raw-data of measured parameters to a magnetic tape. From this tape, the final analysis at the central computer gives the desired tables and plots from an experiment. The data acquisition system includes measurements to obtain:

- pressures (PT)
- differential pressures (dPT)
- temperatures of fluids (TE)
- mass flows (dPT, PT, TE)
- electric currents (I) and voltages (U)
- pump speeds (nT)
- water level positions (CE)
- valve positions

at places shown in the instrumentation diagram, Figure 4.

For recording clad temperatures there were about 100 thermocouples engaged at 16 axial levels of the heated length in the 36-rod bundle.

2.2 The experiment

The preparation of the experiment is initiated several hours before the actual experiment. For the heat-up of the facility, a 200 kW preheater is involved for a period lasting about 5 h. The recirculation pumps are also running during this period. Initial conditions are then established by switching the power supplies to the bundle and

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to the bypass with the 6 MW cooler and the condenser spray in operation. The preheater is now disconnected. For about 10 to 30 minutes, the electric power to the rod bundle and the bypass heating is gradually increased until the initial test conditions are reached. Necessary calibrations are made, and once the equilibrium conditions are approved, the sequence control equipment is activated for break opening, valve manoeuvres, power reduction, pump speed changes and so forth, according to a programmed scheme for the test. For the split break test No. 3051, the transient ends 137 s after opening of the break.

In the present FIX-II experiment, the speed of the pump in the intact recirculation line decreased from the break time to about 20 % of the initial speed at end of the transient. The speed of the broken recirculation line pump was not explicitly controlled.

The break flow escaping through the fast opening break valve, Figure 1, is discharged into the receiving tank, T2. Initially, the tank is partly filled with cold water for efficient pool condensation of the break flow.

The split break assembly consists of a T-piece on the line from pump P2 to the lower plenum. A break flow limiting orifice, downstream of the break isolation valve, consists of an exchangeable conical inlet part followed by a restriction pipe. In experiment No. 3051, the restriction pipe diameter was 6.8 mm corresponding to a 10 % area of one recirculation line.

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Apart from the heat removal from the filler body space, see Chapter 2.1, some 100 kW are also lost by the non-perfect insulation encapsulating the recirculation lines and the pressure vessel. The magnitude of the steady state heat losses was one argument for not performing experiments with very small break areas at FIX-II.

The main measured parameters for the steady state before break are reproduced from Ref (5) in Table 4. The test performance chronology, related to the programming of the sequence control equipment, is given in Table 5.

Experimental raw data were collected for the whole period of the transient. However, internal flows were then only qualified until about 50 s due to uncertainties in the two-phase flow rate measurements.

A summary of the main results (including event times, maximum cladding temperatures and some peak mass flows) is given in Table 6.

2.3 Measurement uncertainty

To obtain estimates for the accuracy of the measured data, test procedures were adapted within the experimental program. Probable errors and errors corresponding to a 95 % confidence level as derived from these tests are summarized in Table 2a. The probable errors of derived quantities, mostly mass flows, are given in Table 2b. The pump speeds are measured using a tachometer of a 1 r/s accuracy. The pump characteristics were verified against the manufacturer's data for cold water single phase operation.

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3 CODE AND MODEL DESCRIPTIONS

The assessment calculation for the FIX-II experiment No. 3051 was done using RELAP5/MOD2, Cycle 36.04. The code was implemented in June 1986 on a CDC computer at the Stockholm Comsource Centre where the calculations were carried through. The descriptive document available for this code at the time of preparing the calculation input was the rather detailed code manual (Ref 7) which also contained an input data manual. The code features are discussed in Chapter 3.1.

Existing FIX-II input for RELAP5/MOD2 (Ref 6) and a previous RELAP5/MOD2 calculation (Ref 8), formed the basis for the present RELAP5/MOD2 input. Details of the input are discussed in Chapter 3.2.

3.1 The Code Features

An extensive code description for the RELAP5/MOD2 is given in (Ref 7). The main characteristics of the code are summarized in Table 3.

Since the RELAP5/MOD2 code is primarily developed for PWR application, the question arises whether the code fails to predict some important features for a BWR-type application like the present FIX-II experiment.

Key questions are, for instance, the behaviour of droplets under top spray cooling, the effects of lower plenum and guide tube flashing on the water distribution in the system, dryout and post dryout phenomena. For experiment 3051 only the effects of mass distribution could be addressed since no dryout was observed in the experiment.

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3.2 The Input Model

The model geometry used in the present calculations is closely related to geometries used in several previous calculations for FIX-II experiments using previous RELAP5/MOD1 code versions (Refs 6 and 8). The nodalization diagram for the geometric modelling used is shown in Figure 5. Figures 6 and 7 depict the modelling in the geometry of the test facility.

To reproduce fundamental measured steady state quantities, see Table 4, the input for the steady state search run got some additional components and control systems:

- I To obtain the steady state dome pressure, a time dependent volume outside of the opened steam relief valve was added. This volume had the experimentally measured dome pressure.
- II The speed of the pumps P1 and P2 was regulated using the RELAP5 control system to reproduce the measured mass flows.
- III To divert the correct mass flow into the core bypass, the junction from the lower plenum was modelled as a motor valve. By trip logic that valve was regulated to give the experimental bypass mass flow. When entering into the transient calculation, the valve setting was fixed.
- IV The measured steam separator collapsed level was satisfied by connecting an auxiliary time dependent volume to the top of the steam separator. The connecting junction was modelled to regulate the collapsed level by water exchange depending of the level offset.

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Evidently, some non-zero flows (points I and IV) will remain at the junctions from the pressure- and level regulating time dependent volumes. These flows are quite small and are influenced by the system heat balance.

The input for the steady state calculation is given in the Appendix A.

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4 THE BASE CASE CALCULATION

The transient calculation of the base case (called Case A) was continued from the restart-plot file obtained from the steady state calculation. To verify the quality of the steady state, the opening of the break was delayed by 30 s.

The calculation of the transient itself was carried out without any particular problems. The smooth lapse of the CPU-time, Plot B.34 and of the computation mass error, Plot B.35 indicate that.

A set of results from the base case calculation and the sensitivity calculations were selected to satisfy the requirement on assessment parameters given in Table 3 of Ref 3. Those parameters are listed in the Table 8 and the corresponding plots reproduced in Appendix B. Since some of the parameters are not available from the measurements, only comparisons between the different calculations are shown in some of the plots. For the mass flow comparisons, it should be pointed out that the experimental data are not reliable after voiding has begun which for most measurements occur 40 to 50 s after break opening time.

The total mass inventory is dependent on the feed and spray water flow, the flow through the relief valve and the break flow. The spray flow and the feed water valves are closed about two seconds after the break. There is a good agreement between calculation and experiment of the mass flow rate through the steam relief valve, Plot B.27. The break mass flow, Plot B.29, which in the experiment is derived from the increasing

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content of a flow receiving tank, Plot B.30, was overpredicted in the base case calculation, particularly up to 45 s. The measured mass flow shows a pronounced peak during the very first seconds after the break. This peak is not realistic and is caused by steam replacing water in the tube leading from the break to the receiving tank. This results in an apparent volume increase equivalent to a water mass of about 37 kg from about 3 s until the end of the test. At the end of the test, the break valve is closed causing refill of the break line. Taking this into account the base case calculation overestimated the mass loss through the break by about 23 kg.

The thermal-hydraulic conditions in the system are also influenced by heat exchange with the core and other boundary structures. Plot B.3 shows the calculated heat exchange with all the passive wall structures in the loop except for the separate filler body space with a known cooling power of about 256 kW. The heat returning from the passive structures exceeds the core decay heat from about 50 s onwards. The structural wall material thickness of the components was generally modelled as 0.09 times the tube inner diameter.

The system pressure, Plots B.20, B.21 and B.33, was well predicted until 40 s. Afterwards the predictions decreased faster than in the experiment. The cycling of the steam relief valve dominates the behaviour of the system pressure.

Flow rates are measured at the bypass inlet, at the discharge sides of the two main pumps and also in the broken loop between break and vessel inlet; these flow rates are depicted in Plots B.22 through B.25. Two additional measurements of

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in-loop mass flows are the differential pressures over the orifice in the steam separator, Plot B.17 and over the core inlet restriction, Plot B.2. The mass flows evaluated from the experiment, i.e. Plots B.22 through B.25, are not reliable after the formation of steam has started at the respective location. The times for the first steam formation range between 40 and 50 s and are indicated by increasing flow oscillations. Up to that time the predicted base case flow rates compare well with the measurements. The flows in the broken loop from the pump side and the lower plenum side, Plots B.24 and B.25, are in agreement with the break flow behaviour.

Plots B.1, B.13 and B.28 show calculated fluid densities at the core bottom, at the reactor vessel bottom and upstream of the break. Fluid densities were not directly measured in the experiment.

At the downcomer bottom, Plot B.18, the first steam is formed at about 40 s when the steam relief valve is opened. The calculation predicts saturation before this point in time. Notice that the thermocouple response may have been affected by structural material. Shortly after 40 s the loop conditions are saturated and the fluid temperatures continue strongly coupled with the pressure.

The fluid inventories of the core, Plot B.12, the upper plenum, Plot B.16, the downcomer, Plot B.14, and of the lower plenum, Plot B.15, are compared as differential pressures which are directly measured in the experiment. The differential pressure over the core is generally

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underpredicted which means that the mass of water in the core was larger than calculated. Underprediction of the friction losses could also have contributed to the discrepancy.

The differential pressure in the lower plenum, Plot B.15, is initially slightly high but is after opening of the steam relief valve reasonably well predicted.

The comparisons of the rod clad temperatures are done at the clad inner surface which is closest to the thermocouple positions of the heated rods in the experiment. The calculated temperatures, Plots B.4 through B.9, agree reasonably well at various levels of the core with the measurements in the experiment except for early and late in the transient. No dryout was ever measured or calculated and heat transfer coefficients typical for two phase cooling provided a strong link between the clad and fluid temperatures. The discrepancies late in the transient were therefore a result of the pressure (and fluid temperature) prediction.

During the steady state and early in the transient the clad temperatures in the experiment appear higher than the predicted temperatures by as much as 10 K. This disagreement is too large to be explained by the thermocouple location in the calculation model.

Heat transfer coefficients (HTC) evaluated from the measurements and calculated HTC are compared in Figure 8. The calculated HTC show a larger variation with time than those obtained from the

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measurements. Since the temperature differences are small the measurement uncertainty could be significant. No definite explanation could be identified for the discrepancy.

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5 SENSITIVITY CALCULATIONS

Although the results from the base case calculation (Case A) compared well with the experiment for many parameters an improved prediction quality could obviously be obtained by adequate input updates.

Case B

The modelling of the present 10 % split break had used a motor valve applying an opening time of 1.2 s known from the experiment. The junction characteristics of that break valve had been a choking model combined with an abrupt area change option. The default value of unity had been applied for the break discharge coefficient.

Case B was run with a break discharge coefficient of 0.76 for subcooled upstream conditions. This value was determined from several sensitivity studies. A discharge coefficient of unity was retained for saturated upstream conditions.

The overall results were generally improved by this change. In particular differential pressures over the core, Plot B.12, over the downcomer, Plot B.14, over the upper plenum, Plot B.16, and over the steam separator, Plot B.17, were in a better agreement with the experiment. Improvements in temperature predictions were also obtained as a consequence of a slightly lower depressurization rate.

Case C

Case C was devoted to modelling of heat exchange with the surroundings. Since this was the smallest break size ever tested in FIX-II it could be expected that the heat exchange could affect the results. Case C used the break discharge coefficients as in the Case B.

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The previously used heat transfer had been determined from steady state conditions. It had been noted that the exact core inlet subcooling was difficult to reproduce. The offset was 2 to 3 K.

To obtain a cooler fluid entering the core the outer surface heat transfer coefficient was split into three coefficients in the ratios of 1:3:9 such that most structures had about the same heat transfer coefficient as earlier. Some structures in the flow path from the feed water inlet to the core inlet, like the pumps and the vessel bottom volume, got the high outer surface heat transfer coefficient. The low heat transfer coefficient was applied on the steam dome structures.

As it turned out this rather large change in the outer surface heat transfer coefficients had a very limited influence on the predicted core inlet subcooling. The steady state fluid temperature decrease down to the core inlet is consequently still not fully explained. The results were nearly identical to that of Case B.

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6 RUN STATISTICS

The transient calculation model used with the base case RELAP5/MOD2 prediction for the FIX-II test No. 3051 was modelled by:

58	volumes
60	junctions
69	heat structures

The volumes number includes two pump components and five time dependent volumes and among the junctions there are two valve components and four time dependent junctions.

The computer efficiency is summarized in Table 7 from the major edit printouts, see also Plot B.34. The table also gives the number of time step reductions from requested time steps forced by the current transport limit in the interval from the previous major edit.

The transient calculation needs were:

Computer time	CPU = 2113. s
Number of time steps	DT = 1278
Number of volumes	C = 58
Transient real time	RT = 145. s

A code efficiency factor of

$$\frac{\text{CPU} \times 10^3}{C \times \text{DT}} = 28.5$$

is obtained, compare Ref 3. The computer used was a Cyber 170-810.

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7 CONCLUSIONS

The present calculation for the FIX-II test No. 3051, a 10 % split break, was the latest out of a series of RELAP5 calculations performed for experiments done with the FIX-II facility. That means that improvements on earlier calculation inputs were incorporated in the input used for the present calculations. The code version used was RELAP5/MOD2, Cycle 36.04.

As in the experiment the calculations showed no dryout during the transient. Comparison of clad temperatures are therefore less meaningful since these are linked to the fluid temperature by large heat transfer coefficients. The major cause for the temperature discrepancies is the slight underprediction of the pressure and thereby the fluid temperatures which are near saturation temperatures towards the end of the test.

The sensitivity studies addressed the discharge coefficient and heat exchange with the surroundings. Changing the discharge coefficient from unity to 0.76 for subcooled blowdown improved the prediction of mass inventory in the core, downcomer, and upper and lower plenum. The sensitivity of the heat exchange with the surroundings did not significantly affect the results.

The mass inventories in the core and downcomer were generally underpredicted in the calculations. The redistribution of mass caused by flashing in lower plenum and guide tubes were correctly predicted by the code.

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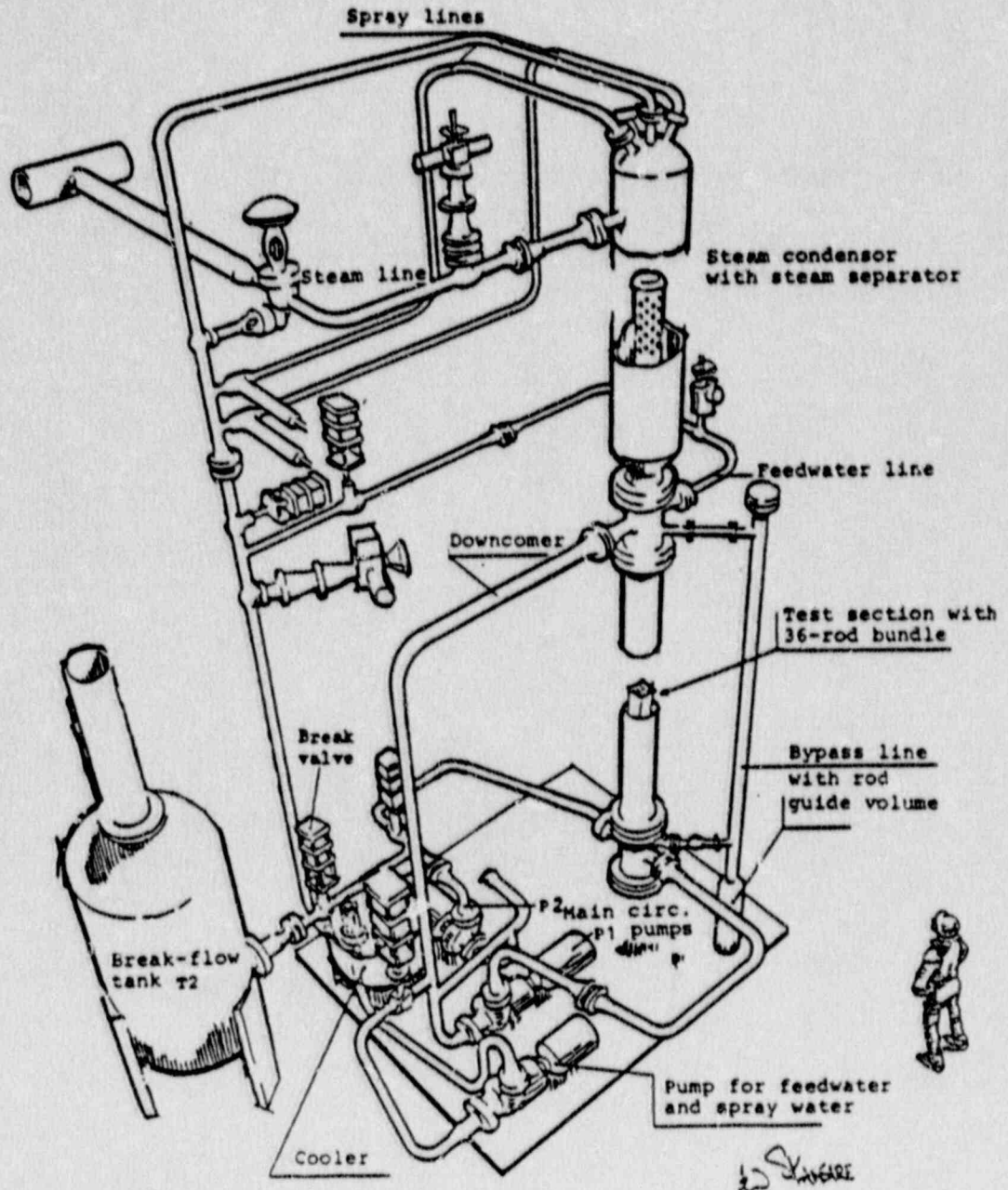


Figure 1

View of the FIX-II facility, condition for split break experiments.

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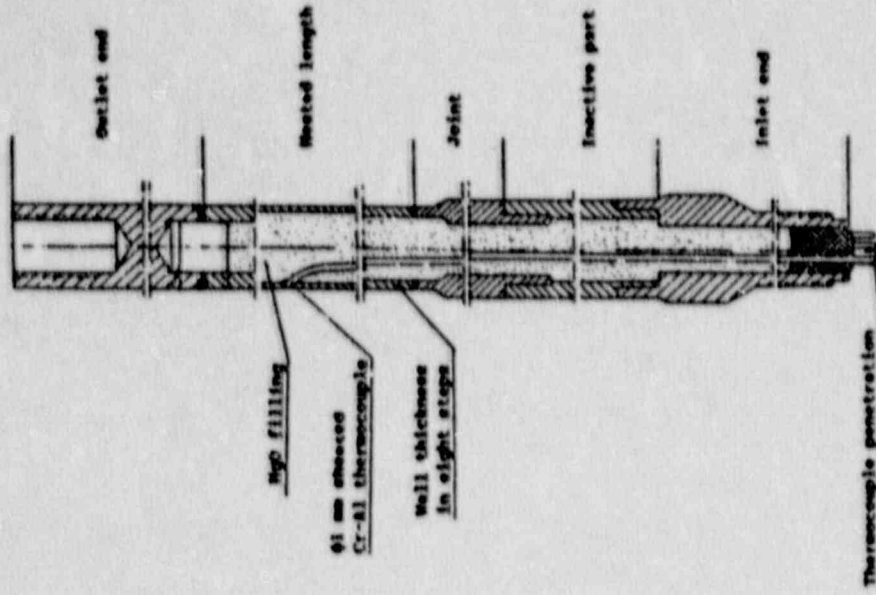


Figure 2b

Design of a fuel rod simulator

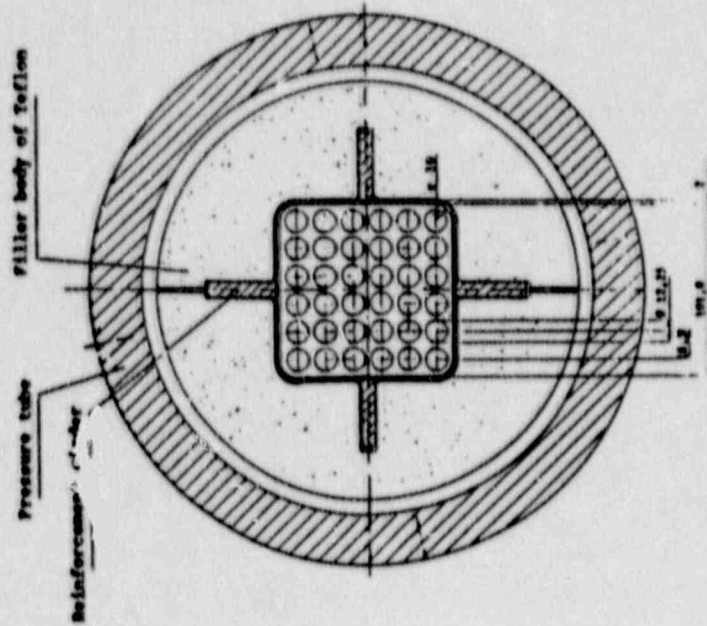


Figure 2a

Cross section of pressure vessel and rod bundle

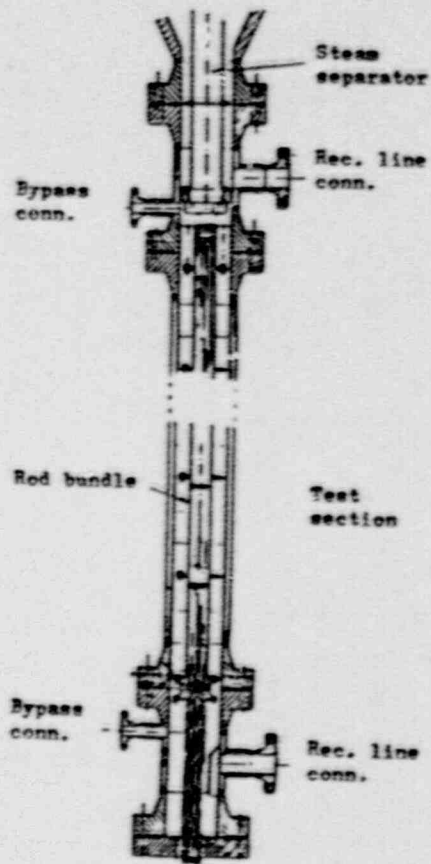


Figure 3a

Lower plenum and core region

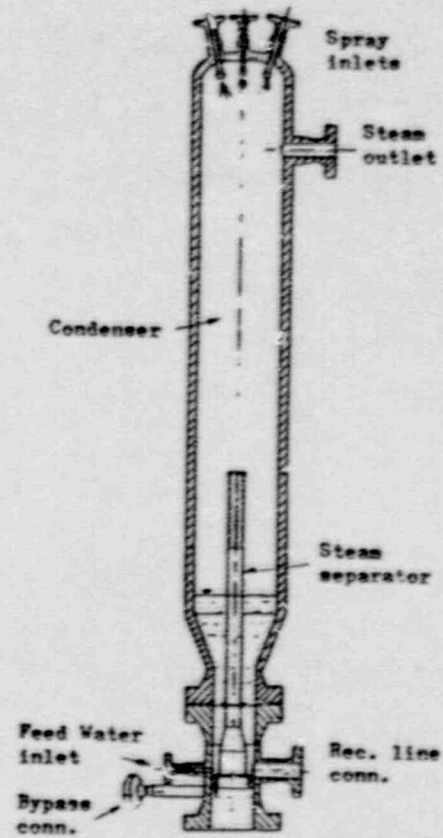


Figure 3b

Steam separator and steam condenser

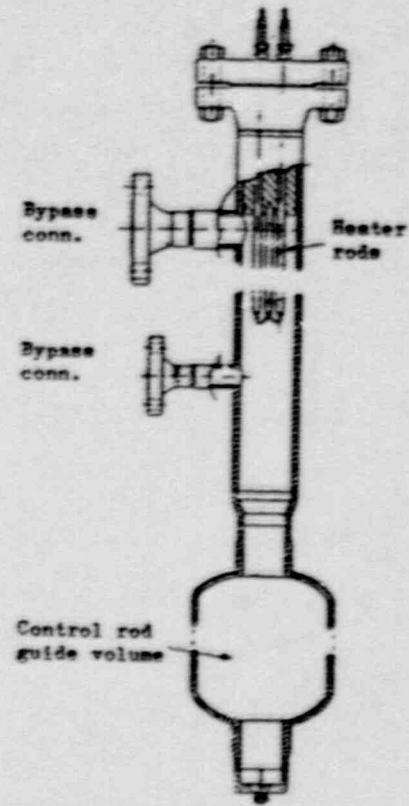


Figure 3c

The external core bypass

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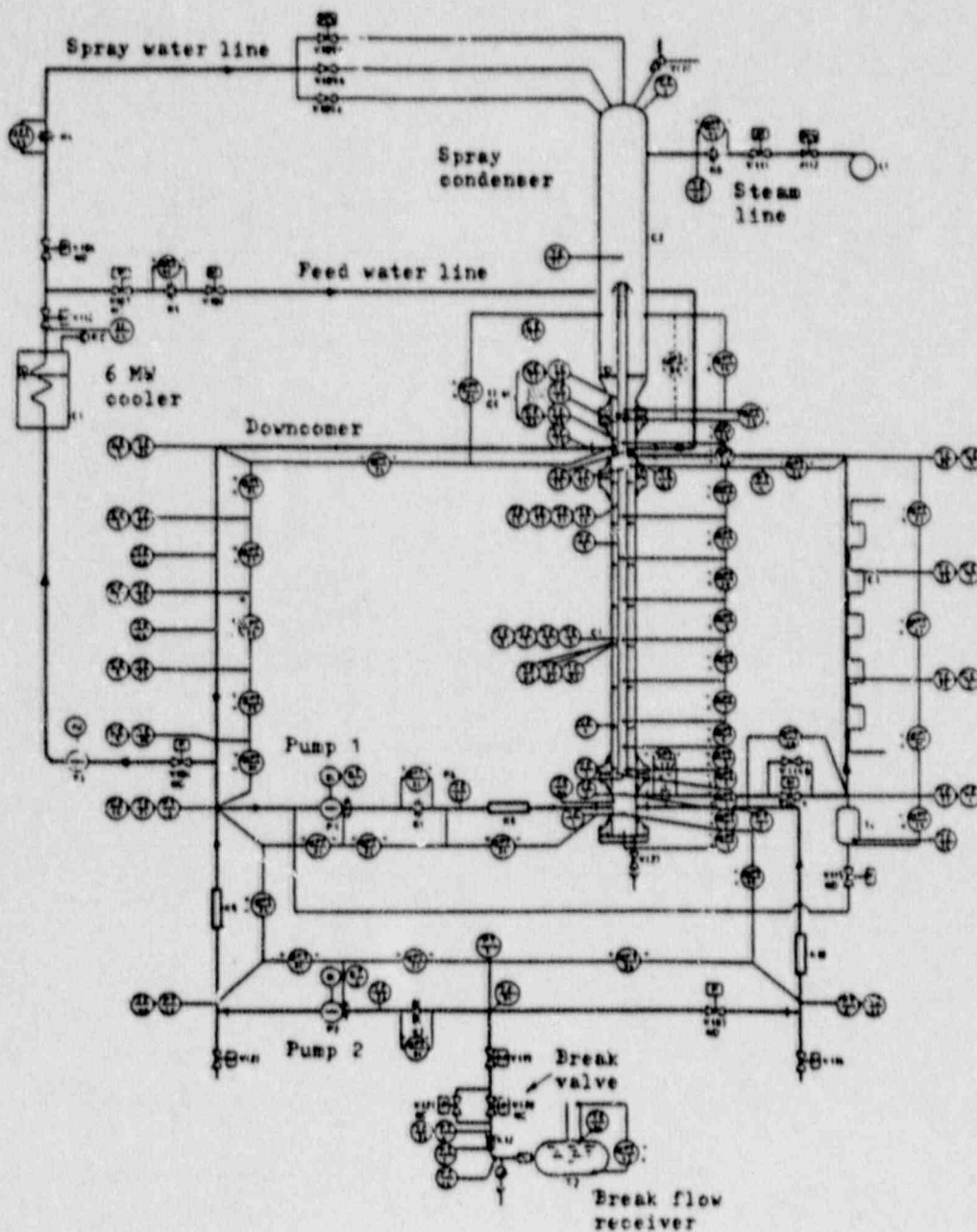


Figure 4

Instrumentation diagram for FIX-11

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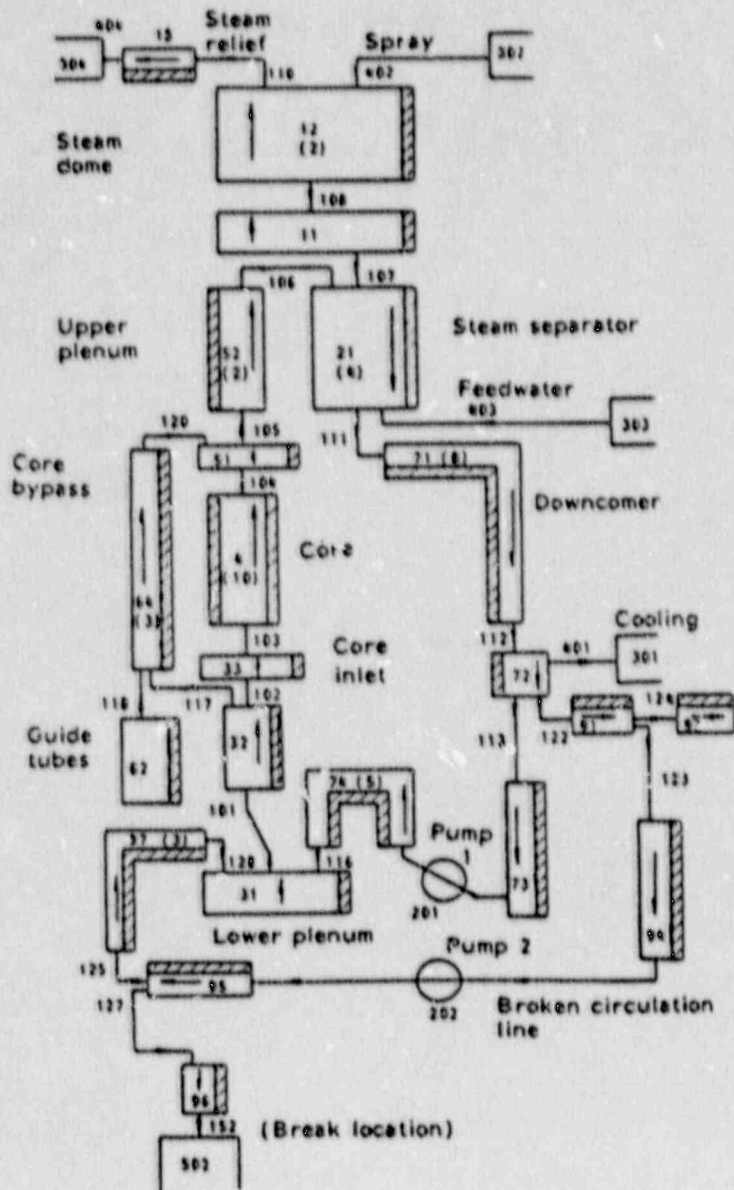


Figure 5

The nodalization diagram for FIX-II

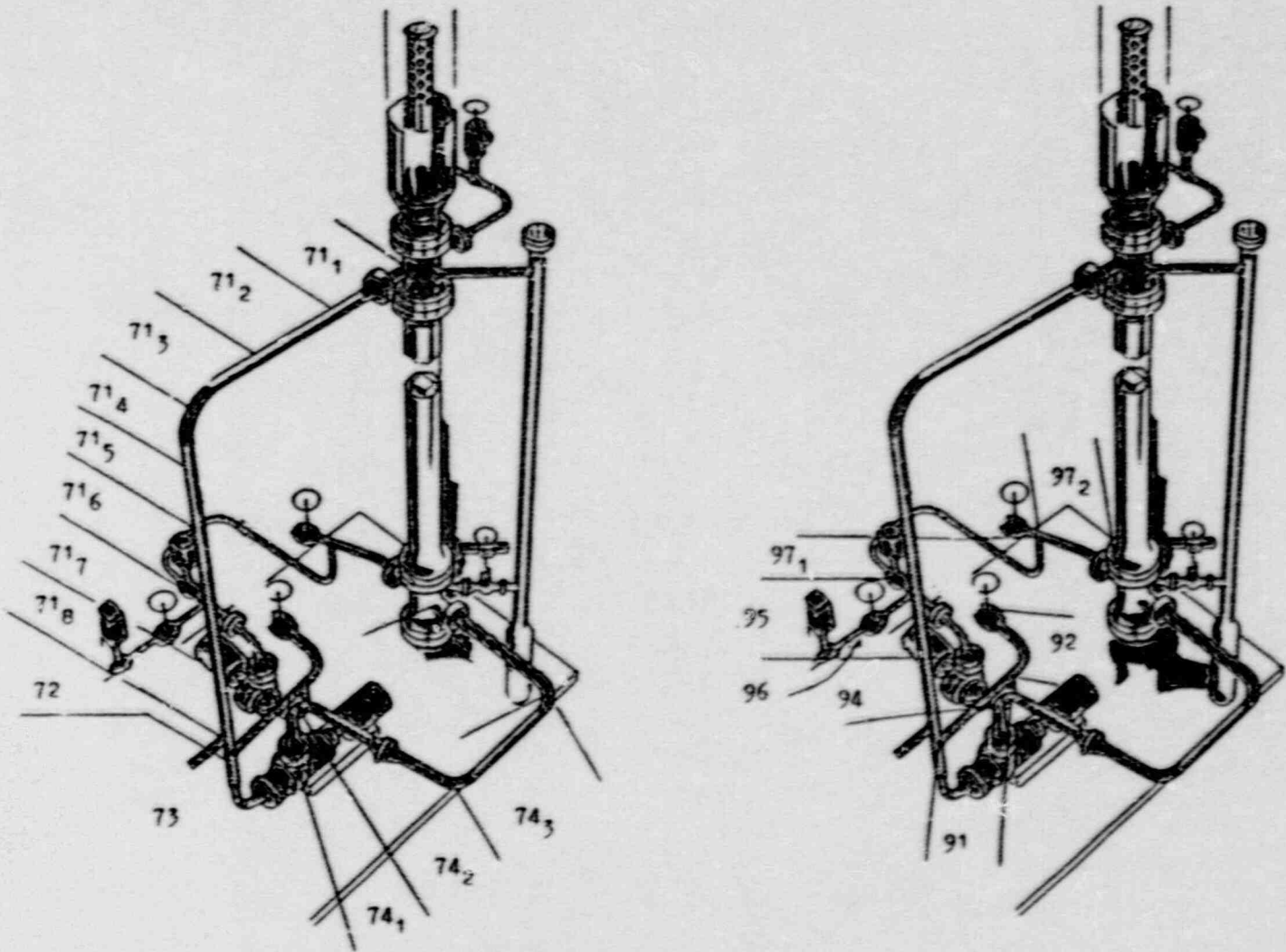


Figure 6
Nodalization of the recirculation lines

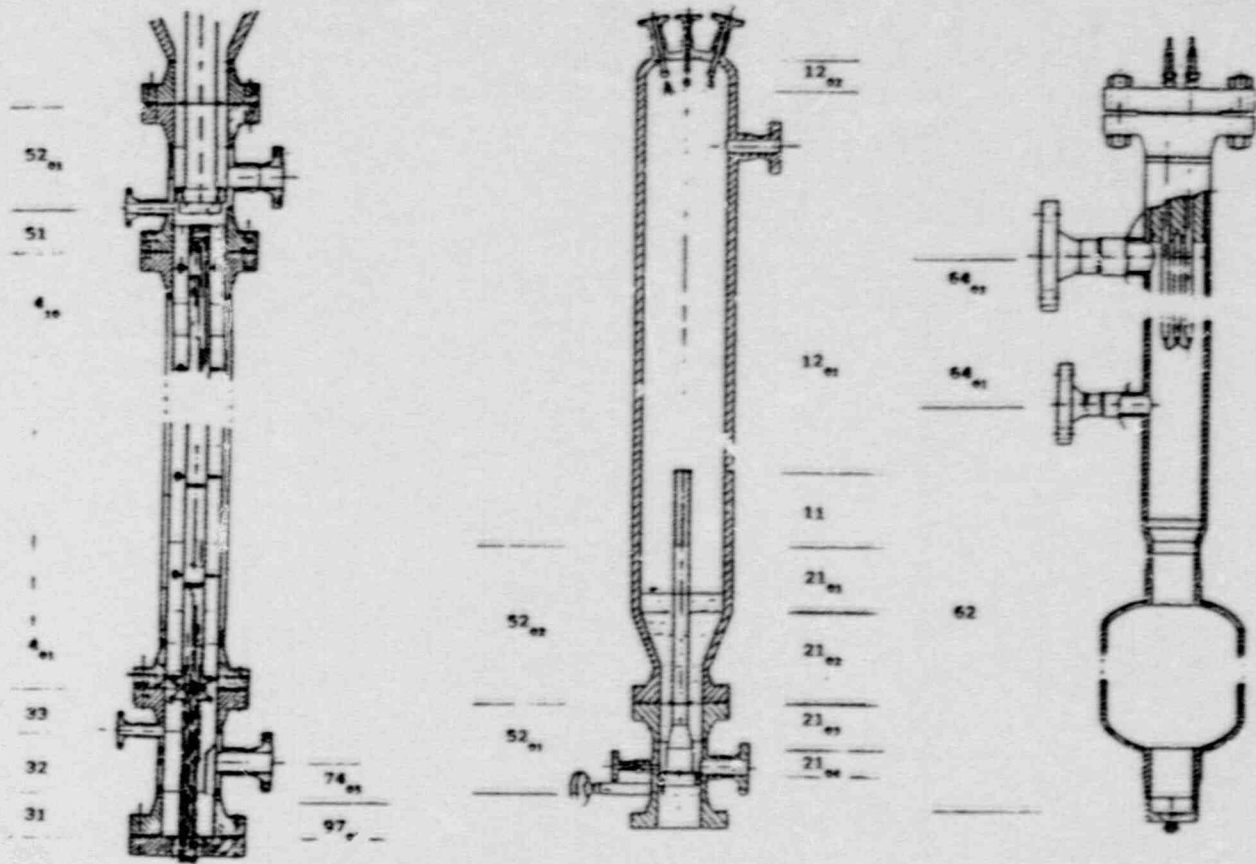


Figure 7

Nodalization of the main volumes of the FIX-II
(compare Figure 3).

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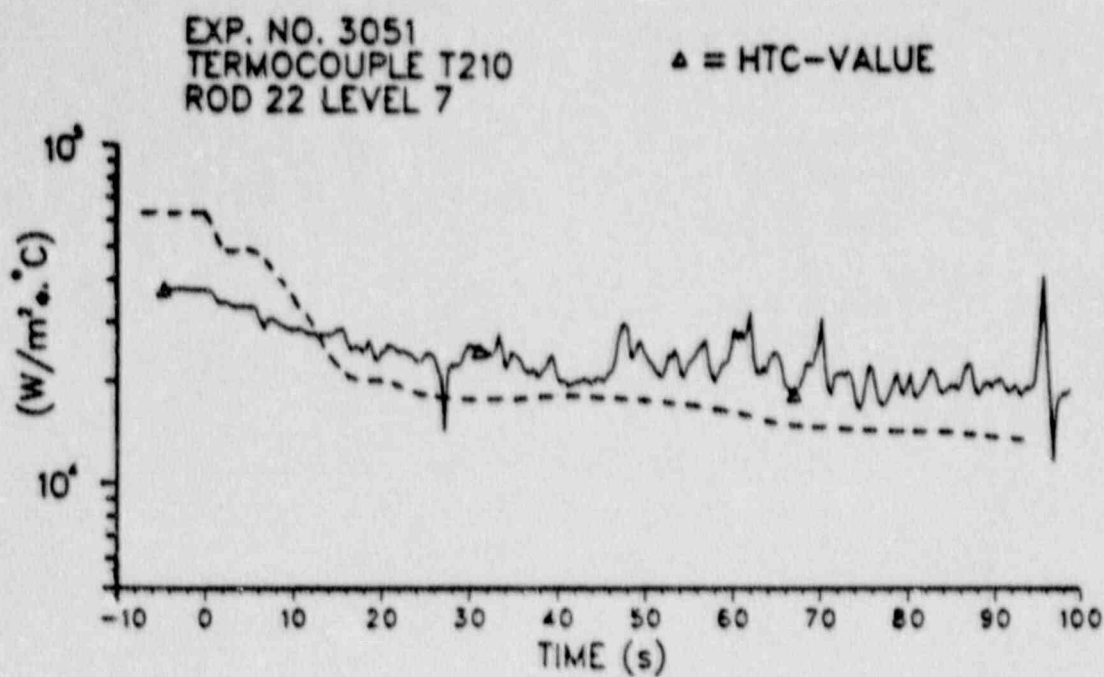


Figure 8

Comparison of heat transfer coefficients at the case model volume 4.05. Dotted line for prediction.

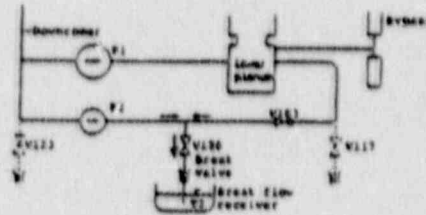
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Table 1

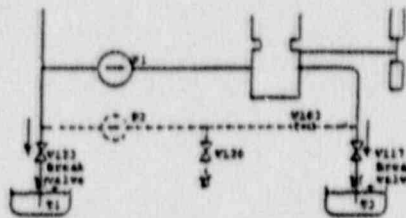
Test matrix of reported FIX-II LOCA tests

Break classification	Split breaks						Guillotine			
	A						B	C		
Type of simulation (see Figure 13)										
Relative break area (%)	10	31	68	100	150	200	155*	200		
Breaks I.D. (mm)	6.8	12.0	15.0	21.6	26.4	30.5	16.0+ 21.6	21.6+ 21.6		
Initial bundle power (MW)										
-hot channel			3.35	3.35					3.35	
-average	2.35	2.35			2.35	2.35	2.35	2.35	2.35	
LOCA test ident. No.	3011	3013	3024 3025 3026 3027	3031	3061	3071	3061	6011	5061	5051 5052

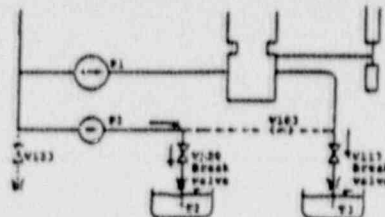
Break type A
Split break



Break type B
Simplified guillotine break



Break type C
Guillotine break



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Table 2.A

Evaluated measurement errors

Quantity	Probable error	Error corresponding to 95 % confidence level
Pressures	0.014 MPa	0.04 MPa
Fluid temperatures	1°C	2°C
Cladding temperatures	1.6°C	3.2°C
Small range differential pressures (5 to 7.5 kPa)	0.13 kPa	0.3 kPa
Medium range differential pressures (25 to 50 kPa)	0.22 kPa	0.5 kPa
High range differential pressures (100 to 700 kPa)	0.26 kPa	0.65 kPa

Table 2.B

Errors in derived quantities

Quantity	Probable error
Mass flow rate in orifice meter K1 (P1)	0.2 kg/s
Mass flow rate in orifice meter K2 (P2)	0.14 kg/s
Mass flow rate in orifice meter K6 (steam flow)	-10 % of actual value
Mass flow rate in orifice meter K7 (Bypass)	-10 % of actual value
Break mass flow rate	-10 % of actual value
Electric power to bundle and bypass heaters	1 % of max value

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Table 3

RELAP5/Mod 2 code features

COMPUTATION PROCESSING FEATURES

- Several problem type and execution control options as
 - a. steady state initialisation using fictitious structure heat capacities for faster convergence
 - b. transient calculation
 - c. strip type execution, to select requested parameters from a restart file
 - d. trip system, to decide on actions during calculation due to reaching specified conditions in calculation parameters.
 - e. ability to delete or add hydrodynamic components, structure components and control variables at a restart of calculation.

CLASSIFICATION OF HYDRODYNAMIC MODEL

- One-dimensional, with provisions for
 - a. choked flow model
 - b. abrupt area change model
 - c. cross flow junctions.
- Two-fluid, six equation, space-time numerical solution scheme.
- flow regime oriented field characteristics depending on mass flux and void fraction for
 - a. horizontal flow with bubbly, slug, mist and stratified fields
 - b. vertical flow with bubbly, slug, annular-mist (and stratified) fields
 - c. high mixing flow with bubbly and mist fields (for pumps).

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Table 3 con'tHYDRODYNAMIC COMPONENTS (Input systematics)

- Volume type components
 - a. single volume
 - b. pipe and annulus, for condensed input of several similar single volumes
 - c. time dependent volume, for defining a boundary source with a time dependent fluid state
 - d. branch, a volume capable of two or more connecting junctions at either end
 - e. pump, characterized by rated values for flow, head, torque, density and moment of inertia. The single phase homologous curve, two-phase multipliers and phase difference tables to model the dynamic pump behaviour
 - f. special system components for steam separator, jetmixer, turbine and accumulator.
- Junction type components
 - a. single junction
 - b. time dependent junction, for a time dependent junction flow with a time dependent or controlled flow state
 - c. cross-flow junction, to model a small cross flow, a tee branch or a small leak flow
 - d. valve, various operation characteristics available for check valve, trip valve, inertial valve and relief valve.

INTERPHASE CONSTITUTIVE EQUATIONS

- Interphase drag
 - a. steady drag due to viscous shear depending on flow regime. Semi-empirical mechanisms to describe flow regime transitions
 - b. dynamic drag due to virtual mass effect.
- Interphase mass and heat transfer depending on flow regime and the fluid fields to saturation temperature differences

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Table 3 con'tFLUID TO WALL CONSTITUTIVE EQUATIONS

- Wall friction due to wall shear effects formulated for flow regimes and based on a two-phase multiplier approach.
- Wall heat transfer depending on flow characteristics defined for
 - a. single-phase forced convection (Dittus-Boelter)
 - b. saturated nucleate boiling (Chen)
 - c. subcooled nucleate boiling (modified Chen)
 - d. critical heat flux (Biasi or modified Zuber)
 - e. transition film boiling (Chen)
 - f. film boiling (Bromley-Pomeranz and Dougall-Rohsenow)
 - g. condensation (partly Dittus-Boelter).
- Interfacial mass transfer at the wall depending on wall, fluid and saturation temperatures for
 - a. subcooled and saturated boiling
 - b. transition film and film boiling
 - c. condensation.

HEAT STRUCTURES

These may be rectangular, cylindrical or spherical in shape. The structure position is defined through component numbers of left and right hand side hydraulic components. A structure is physically defined by the geometry and the temperature dependent conductivity and volumetric heat capacity data. The structure model is further specified by the number of internal mesh points in the direction of heat flow.

CONTROL COMPONENTS

By these new (control) variables are defined from calculated parameters using algebra, standard functions, trip type operands or integrals.

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Table 4

Initial conditions, for test No. 3051

Quantity		Measured	Predicted		
			Case A	Case B	Case C
Pressure in the steam dome	(MPa)	6.99	6.99	6.99	6.99
Power to the 36-rod bundle (incl connections)	(MW)	2.38	2.38	2.38	2.38
Power to the bypass heaters	(kW)	61.1	61.1	61.1	61.1
Cooling power in the filler body space	(kW)	256.	255.	255.	255.
Mass flow rate through pump P1	(kg/s)	4.85	4.85	4.85	4.90
Mass flow rate through pump P2	(kg/s)	1.59	1.59	1.59	1.62
Mass flow rate in the bypass	(kg/s)	.69	.69	.69	.71
Mass flow rate in the 36-rod bundle	(kg/s)	5.75	5.75	5.75	5.81
Mass flow rate in the spray line	(kg/s)	3.08	3.08	3.08	3.08
Mass flow rate in the feed water line	(kg/s)	1.95	1.95	1.95	1.95
Temperature of water at the bundle inlet	(C)	267.	268.	268.	268.
Temperature of feed and spray water	(C)	179.	179.	179.	179.
Water level in the spray condenser	(m)	.835	.836	.836	.834
Rotational speed of pump P1	(/s)	24.63	25.44	25.44	25.43
Rotational speed of pump P2	(/s)	31.64	33.39	33.39	33.36
Head of pump P1	(kPa)	118.6	123.5	123.5	123.3

Table 5

List of events in test No 3051

Event	Imposed action	System reaction	Time (s)		
			Case A	Case B	Case C
The break occurs (valve V120 starts to open)	.0		.0	.0	.0
Start of coast down of pump P1	.0		.0	.0	.0
Start of power decay (rod bundle and bypass)	.0		.0	.0	.0
The SRV starts to open	.5		.5	.5	.5
The SRV is fully open	1.1		1.1	1.1	1.1
The SRV starts to close	1.5		1.5	1.5	1.5
Minimum in steam dome pressure occurs		1.9	2.	2.	2.
The spray flow is closed	2.0		2.0	2.0	2.0
The feed water flow is closed	2.1		2.1	2.1	2.1
Valve V104 to the evaporation cooler is closed	2.2		2.2	2.2	2.2
The SRV is closed	2.8		2.8	2.8	2.8
Maximum of steam dome pressure		8.9	8.5	9.0	8.5
Flow reversal in the intact RCL		20.	18.5	19.5	19.5
The SRV starts to open	39.6		39.6	39.6	39.6
The SRV is fully open	40.3-137.2		40.3	40.3	40.3
Cavitation in the broken RCL pump P2		45.	44.	45.	46.
Flashing starts in the LP (at saturation)		45.	45.	45.	45.
Level swell (recovery) in the downcomer		45.	44.	45.	46.
Flashing starts in the bypass guide tubes volume		49.6	52.	53.	53
Peak in the bypass flow into the UP		51.	55.	55.	56.
Test stop signal	136.1		-	-	-

Abbreviations: LP = Lower plenum
 UP = Upper plenum
 RCL = Recirculation line
 SRV = Steam relief valve

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Table 6

Summary of the main results in test No 3051

	Measured	Predicted		
		Case A	Case B	Case C
Total time of transient (break discharge) (s)	136.1	-	-	-
Initial dryout	None	- - None - -		
Bundie uncover	Not achieved	- - Not achieved - -		
Break mass flow 2 s after the break * (kg/s)	2.7	2.	2.0	2.0
Max. break flow rate from lower plenum (kg/s)	<1.	.6	<.0	<.0
Max. break flow through pump P2 (kg/s)	2.7	2.5	2.5	2.5
Max. dome pressure after break time (MPa)	7.10	7.14	7.17	7.18
Dome pressure at the end of test (Mpa)	(2.04)	1.81	1.97	1.92
Max. rod temperature, end of blowdown (C)	227.	229.	216.	219.
Integrated break mass flow (kg)	110.	138.	119.	121.
Integrated steam relief mass flow (kg)	52.	50.	52.	51.

* Approx. at the maximum break flow of the test

Table 7

Run statistics data (Case A)

Time (s)	Computer CPU time (s)	No. of time steps	No. of time step reductions in interval				
			quality	extrap.	mass	propy.	Courant
-30.	-679.	-480	-	-	-	-	-
0.*	0.	0	0	0	0	0	0
10.	234.	160	0	0	0	0	0
30.	572.	393	1	0	1	0	0
60.	1182.	776	2	0	2	0	0
100.	1663.	1030	18	0	3	12	71
145.	2113.	1278	3	0	5	0	65

* Time of break opening

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Table 8

Parameters plotted and used in the assessment comparison.

COMPONENT	CONTINUED PARAMETER *	EXPOSURE (IDENTIFIER)	PREDICTION (MINOR UNIT)	PLOT IDENTIF.		PLOT NO.	
				EXP.	CALC.		
CORE	FLUID DENSITY, BOTTOM	***	BD0 04.01		BD17	B. 1	
	MASS FLOW RATE, INLET *	DPT 4	P 33.01 - P04.01	D 4	PD47	B. 2	
	HEATING POWER	X 001	CHTOLVAD 57	D001	SP17	B. 3	
	CLAD TEMPERATURE, LEVEL 1	TE 191, TE 204, TE 211, TE 246	HTTEMP 4.0100	TC 1	HT17	B. 4	
	.. . LEVEL 3	TE 104, TE 183, TE 243, TE 240	HTTEMP 4.0300	TC 3	HT37	B. 5	
	.. . LEVEL 5	TE 202, TE 227, TE 232, TE 237, TE 252	HTTEMP 4.0400	TC 5	HT57	B. 6	
	.. . LEVEL 9	TE 102, TE 137, TE 167, TE 172, TE 187, TE 197, TE 272	HTTEMP 4.0600	TC 9	HT97	B. 7	
	.. . LEVEL 12	TE 118, TE 123, TE 128, TE 148, TE 220	HTTEMP 4.0700	TC12	HT57	B. 8	
	.. . LEVEL 15	TE 175, TE 190, TE 275	HTTEMP 4.1000	TC15	HT67	B. 9	
	INLET TEMPERATURE	TE 3	TEMPF 33.01	T 3	TF17	B. 10	
	OUTLET TEMPERATURE	TE 14	TEMPF 51.01	T 14	TF27	B. 11	
	CORE INVENTORY *	DPT 5 + DPT 6 + DPT 7 + DPT 8 + DPT 9 + DPT 10 + DPT 11 + DPT 12	P 04.01 - P 51.01 **	D CO	PDC7	B. 12	
	VESSEL	FLUID DENSITY, BOTTOM	***	BD0 31.01		BD27	B. 13
		DOWNCOMER MASS INVENTORY *	DPT 27 + DPT 28 + DPT 29 + DPT 30	P 71.03 - P 72.01 **	D BC	PDC7	B. 14
LOWER FLESH MASS INVENTORY *		DP 2 + DP3 + DP 1	P 31.01 - P 32.01 **	D LP	PDL7	B. 15	
UPPER FLESH MASS INVENTORY *		DP 13 + DP 14	P 51.01 - P 52.01 **	D UP	PDU7	B. 16	
PRESSURE LOSS, S.S. ORIFICE		DP 54	P 52.01 - P 52.02	D 54	PDL7	B. 17	
DOWNCOMER TEMPERATURE, BOTTOM		TE 31	TEMPF 71.04	T 31	TF37	B. 18	
UPPER FLESH TEMPERATURE		TE 15	TEMPF 52.01	T 15	TF47	B. 19	
LOWER FLESH PRESSURE		PT 3	P 31.01	P 3	P 17	B. 20	
UPPER FLESH PRESSURE		PT 4	P 52.01	P 4	P 27	B. 21	
MASS FLOW RATE, BYPASS		X 602	WFLOWJ 117	X602	WF17	B. 22	

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COMPONENT	CONDITIONS PARAMETER *	EXPERIMENT (IDENTIFIED)	PREDICTION (RLENG EDIT)	PLOT IDENTIF		PLOT NO.
				EXP.	CALC.	
RECIRCULATION LINE	MASS FLOW RATE, I. L. PUMP (OSIPIC0 01)	X 603	OPLOWJ 201.02	S603	OP27	B.23
	MASS FLOW RATE, D. L. PUMP (OSIPIC0 02)	Z 604	OPLOWJ 202.02	S604	OP37	B.24
	MASS FLOW RATE, S. L. VESSEL INLET (SPOOL PIECE R10)	X 610	OPLOWJ 07.02	S610	OP47	B.25
SYSTEM	MASS INVENTORY	***	THASS		MA77	B.26
	MASS FLOW RATE, STEAM RELIEF	X 607	OPLOWJ 607	S607	MP57	B.27
	HEAT LOSS, PASSIVES	***	CTRLVAR 53		HL17	B.3
BREAK	FLUID DENSITY	***	RRO 96.01		RK37	B.28
	MASS FLOW RATE	X 636	OPLOWJ 152	S636	MP67	B.29
	MASS FLOW RATE, INTEGRATED	X 661	CTRLVAR 55	S661	ML17	B.30
	INLET TEMPERATURE	TE 34	TEMPF 96.01	T 34	TF57	B.31
	INLET SUBCOOLING	***	TEMPC 96.01 - TEMPF 96.01		TSU7	B.32
	INLET PRESSURE	PT 6	P 96.01	P 6	P 37	B.33
RELAPS/MOD2	COMPUTATION CPU TIME	***	CPUTIME		CPU7	B.34
	COMPUTATION MASS ERROR	***	DMASS		MAE7	B.35

* THE COMPARISON PARAMETERS ARE THOSE REPORTED AS DIRECTLY MEASURED
OR AS COMPUTED RESULTS FROM THE EXPERIMENT.
PRESSURE DIFFERENCE INSTEAD OF MASS FLOW RATE OR OF MASS INVENTORY.

** CORRECTIONS APPLIED TO RESUME THE CORRECT PRESSURE SENSOR LEVELS.

*** NO DATA AVAILABLE FROM THE EXPERIMENT.

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Address	Label	Value	Unit	Address	Label	Value	Unit
4010100	1	0.00	D	20110000	MELT FLOW	45.38	D
4010101	2	0.00	D	20110001	MELT CONTROL VAR 99	0.00	D
4010102	3	0.00	D	20110002	1.00	1.00	D
4010103	4	0.00	D	20110003	1.00	1.00	D
4010104	5	0.00	D	20110004	1.00	1.00	D
4010105	6	0.00	D	20110005	1.00	1.00	D
4010106	7	0.00	D	20110006	1.00	1.00	D
4010107	8	0.00	D	20110007	1.00	1.00	D
4010108	9	0.00	D	20110008	1.00	1.00	D
4010109	10	0.00	D	20110009	1.00	1.00	D
4010110	11	0.00	D	20110010	1.00	1.00	D
4010111	12	0.00	D	20110011	1.00	1.00	D
4010112	13	0.00	D	20110012	1.00	1.00	D
4010113	14	0.00	D	20110013	1.00	1.00	D
4010114	15	0.00	D	20110014	1.00	1.00	D
4010115	16	0.00	D	20110015	1.00	1.00	D
4010116	17	0.00	D	20110016	1.00	1.00	D
4010117	18	0.00	D	20110017	1.00	1.00	D
4010118	19	0.00	D	20110018	1.00	1.00	D
4010119	20	0.00	D	20110019	1.00	1.00	D
4010120	21	0.00	D	20110020	1.00	1.00	D
4010121	22	0.00	D	20110021	1.00	1.00	D
4010122	23	0.00	D	20110022	1.00	1.00	D
4010123	24	0.00	D	20110023	1.00	1.00	D
4010124	25	0.00	D	20110024	1.00	1.00	D
4010125	26	0.00	D	20110025	1.00	1.00	D
4010126	27	0.00	D	20110026	1.00	1.00	D
4010127	28	0.00	D	20110027	1.00	1.00	D
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4010198	99	0.00	D	20110098	1.00	1.00	D
4010199	100	0.00	D	20110099	1.00	1.00	D

15.1

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30201400 MTC-T 7.0
30201401 0.0
30201500 MTC-T 21.0
30201600 MTC-T 21.0
30201601 0.0
30201602 83.0

END

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Data comparison plots

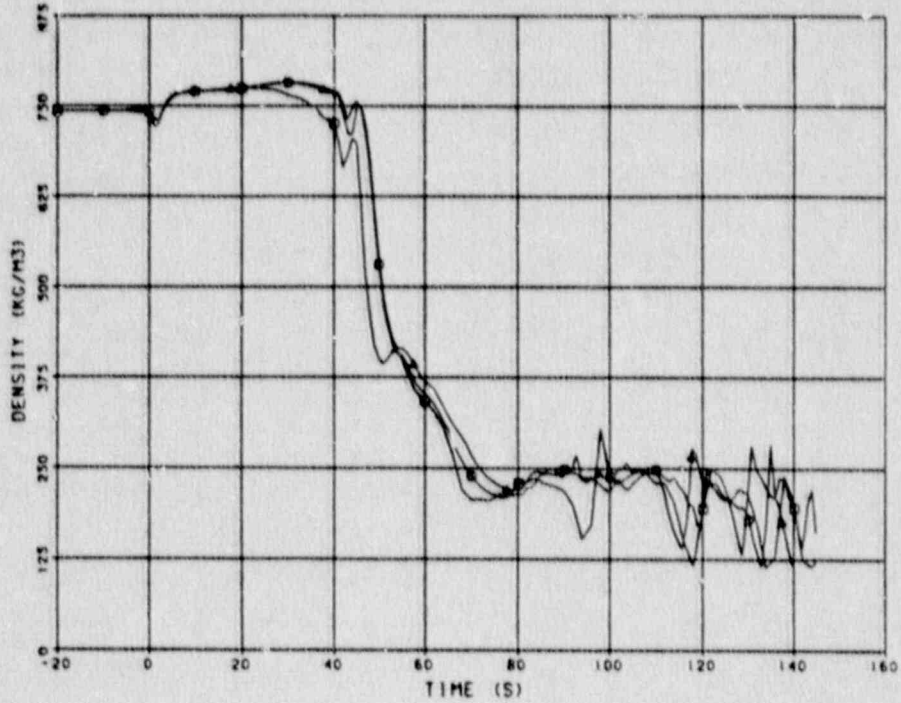
PLAT NO.	IDENT.	QUANTITY	(EXPERIMENT)	(CALCULATIONS)
8.1	8K17	FLUID DENSITY	CASE BOTTOM (END 5481) CASE 7	
8.2	8.4 8P17	DIFF. PRESSURE DIFF. PRESSURE	CASE INLET RESTRICTION (OPT 4) - EXPERIMENT CASE INLET RESTRICTION (P 3101 - P 401) CASE 7	
8.3	8K01 8L17	ELECTRIC POWER HEAT LOSS FROM PASSIVES (CONTROLLER 57)	CASE - EXPERIMENT CASE 7	
8.4	8C 2 8T17	MEAN CLAD TEMP. MEAN CLAD TEMPERATURE	LEVEL 1 (7191 7204 7211 7246) - EXPERIMENT LEVEL 1 (RTTOWP 401000105) CASE 7	
8.5	8C 3 8T27	MEAN CLAD TEMP. MEAN CLAD TEMPERATURE	LEVEL 3 (7104 7183 7243 7246) - EXPERIMENT LEVEL 3 (RTTOWP 403000105) CASE 7	
8.6	8C 5 8T37	MEAN CLAD TEMP. MEAN CLAD TEMPERATURE	LEVEL 5 (7202 7227 7232 7237) - EXPERIMENT LEVEL 5 (RTTOWP 404000105) CASE 7	
8.7	8C 9 8T47	MEAN CLAD TEMP. MEAN CLAD TEMPERATURE	LEVEL 9 (7102 7137 7167 7177 7187 7197) - EXPERIMENT LEVEL 9 (RTTOWP 406000105) CASE 7	
8.8	8C12 8T57	MEAN CLAD TEMP. MEAN CLAD TEMPERATURE	LEVEL 12 (7118 7123 7138 7148 7122) - EXPERIMENT LEVEL 12 (RTTOWP 407000105) CASE 7	
8.9	8C15 8T67	MEAN CLAD TEMP. MEAN CLAD TEMPERATURE	LEVEL 15 (7175 7190 7275) - EXPERIMENT LEVEL 15 (RTTOWP 410000105) CASE 7	
8.10	8.7 8T77	P 10 TEMPERATURE FLUID TEMPERATURE	CASE INLET (7E 3) - EXPERIMENT CASE INLET (TEMP 3101) CASE 7	
8.11	8.14 8T27	FLUID TEMPERATURE FLUID TEMPERATURE	CASE OUTLET (7E 14) - EXPERIMENT CASE OUTLET (TEMP 5101) CASE 7	
8.12	8.10 8P07	DIFF. PRESSURE DIFF. PRESSURE	CASE (OPT 5 - OPT 6 - ... - OPT 12) - EXPERIMENT CASE (FROM P 401 - P 5101) CASE 7	
8.13	8K27	FLUID DENSITY	VESS. BOTTOM (END 3101) CASE 7	
8.14	8.10 8P07	DIFF. PRESSURE DIFF. PRESSURE	DOWNCOMER (OPT 27 - ... - OPT 30) - EXPERIMENT DOWNCOMER (FROM P 7103 - P 7201) CASE 7	
8.15	8.1P 8P07	DIFF. PRESSURE DIFF. PRESSURE	LOWER PLENUM (OPT 2 - OPT 3 - OPT 5) - EXPERIMENT LOWER PLENUM (FROM P 3101 - P 3301) CASE 7	
8.16	8.1P 8P07	DIFF. PRESSURE DIFF. PRESSURE	UPPER PLENUM (OPT 13 - OPT 14) - EXPERIMENT UPPER PLENUM (FROM P 3101 - P 3201) CASE 7	
8.17	8.14 8P07	DIFF. PRESSURE DIFF. PRESSURE	STEAM SEPARATOR ORIFICE (OPT 54) - EXPERIMENT STEAM SEPARATOR ORIFICE (P 5201 - P 5202) CASE 7	
8.18	8.18 8T37	FLUID TEMPERATURE FLUID TEMPERATURE	DOM. CORN. BOTTOM (7E 31) - EXPERIMENT DOWNCOMER BOTTOM (TEMP 7108) CASE 7	
8.19	8.15 8T37	FLUID TEMPERATURE FLUID TEMPERATURE	UPPER PLENUM (7E 15) - EXPERIMENT UPPER PLENUM (TEMP 5107) CASE 7	
8.20	8.5 8P 17	PRESSURE PRESSURE	LOWER PLENUM (PT 3) - EXPERIMENT LOWER PLENUM (P 3101) CASE 7	
8.21	8.6 8P 27	PRESSURE PRESSURE	UPPER PLENUM (PT 4) - EXPERIMENT UPPER PLENUM (P 5201) CASE 7	
8.22	8A02 8P27	MEAN FLOW RATE MEAN FLOW RATE	UPPER - EXPERIMENT UPPER (REFLOW 117) CASE 7	
8.23	8A03 8P27	MEAN FLOW RATE MEAN FLOW RATE	I.L. PUMP - EXPERIMENT I.L. PUMP (REFLOW 20103) CASE 7	
8.24	8A04 8P37	MEAN FLOW RATE MEAN FLOW RATE	B.L. PUMP - EXPERIMENT B.L. PUMP (REFLOW 20203) CASE 7	
8.25	8A10 8P47	MEAN FLOW RATE MEAN FLOW RATE	B.L. VESSEL INLET (REFLOW 20303) - EXPERIMENT B.L. VESSEL INLET (REFLOW 20403) CASE 7	
8.26	8A27	TOTAL MASS	IN SYSTEM CASE 7	
8.27	8A07 8P57	MEAN FLOW RATE MEAN FLOW RATE	STEAM HEATER - EXPERIMENT STEAM HEATER (REFLOW 404) CASE 7	
8.28	8A27	PLUO DENSITY	MEAN (END 5401) CASE 7	
8.29	8A36 8P67	MEAN FLOW RATE MEAN FLOW RATE	STEAM PUMP T4 TEMPERATURE - EXPERIMENT STEAM PUMP T4 (REFLOW 153) CASE 7	
8.30	8A71 8L37	MEAN MASS MEAN TOTAL MASS LOSS	CONTROLLER 55) CASE 7	
8.31	8.34 8P57	FLUID TEMPERATURE FLUID TEMPERATURE	MEAN INLET (7E 34) - EXPERIMENT MEAN INLET (TEMP 5A01) CASE 7	
8.32	8A07	DOWNCOMER	MEAN INLET (TEMP 5101) - EXPERIMENT DOWNCOMER (FROM P 7103 - P 7201) CASE 7	
8.33	8.6 8P 17	PRESSURE PRESSURE	MEAN INLET (PT 4) - EXPERIMENT MEAN INLET (P 5201) CASE 7	
8.34	8A07	CRITIQUE	CASE 7	
8.35	8A07	MEAN MASS	LOSS CASE 7	

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RELAP5/MOD2 CALCULATION FOR FIX-II, EXP 3051

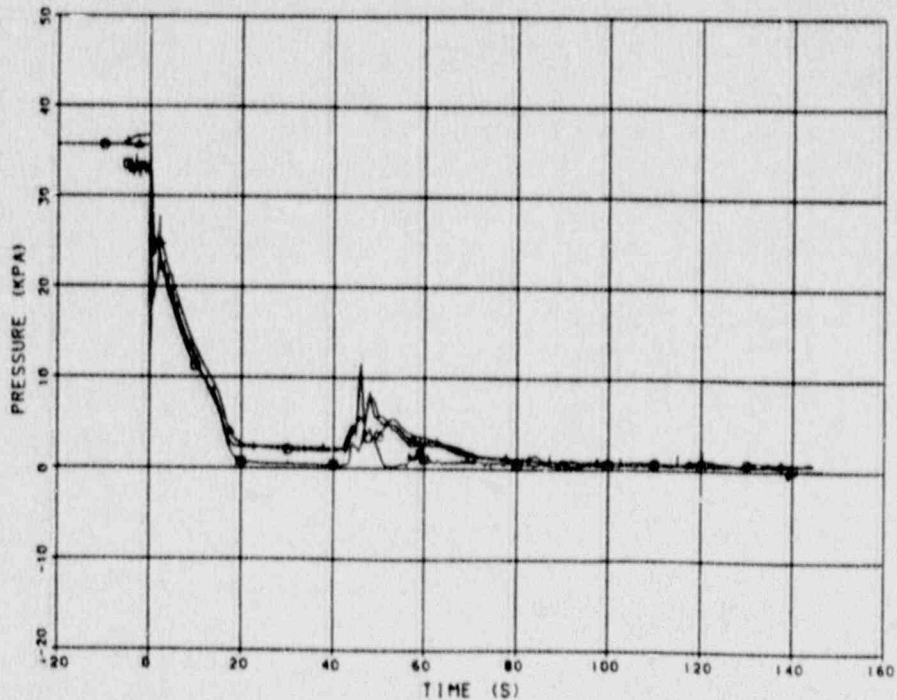
4 0 0 FLUID DENSITY, CORE BOTTOM (RHO 0401) CASE A
 FLUID DENSITY, CORE BOTTOM (RHO 0401) CASE B
 FLUID DENSITY, CORE BOTTOM (RHO 0401) CASE C

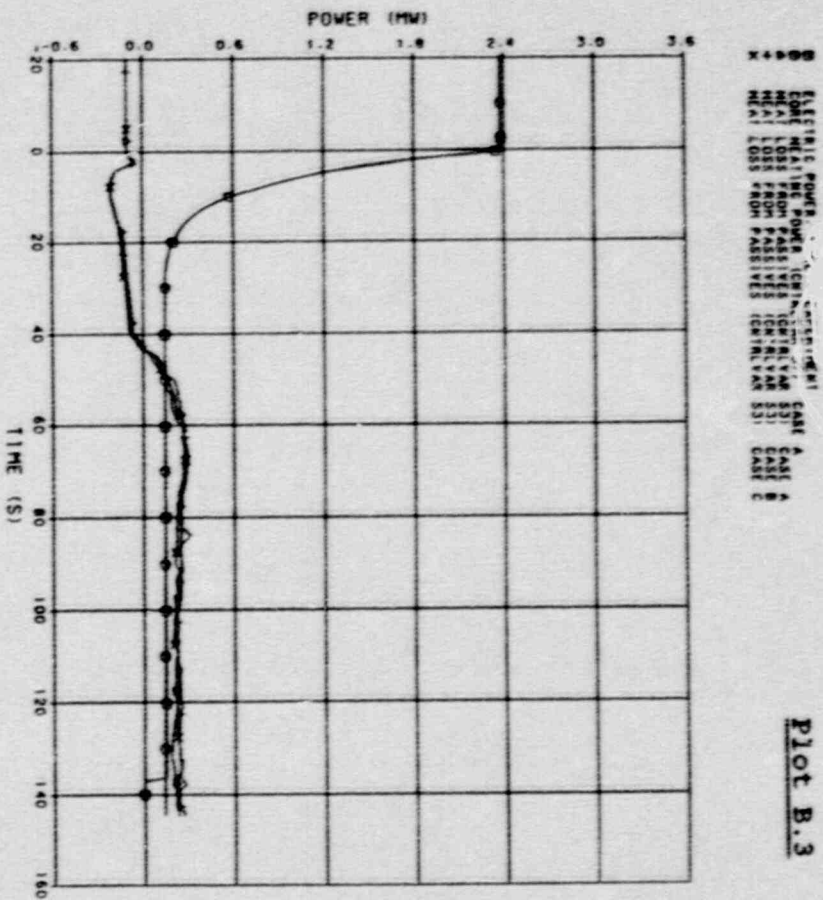
Plot B.1



4 4 0 0 DIFF. PRESSURE, CORE INLET RESTRICTION (DPT 4) - EXPERIMENT
 DIFF. PRESSURE, CORE INLET RESTRICTION (P 3301 - P 401) CAS
 DIFF. PRESSURE, CORE INLET RESTRICTION (P 3301 - P 401) CAS
 DIFF. PRESSURE, CORE INLET RESTRICTION (P 3301 - P 401) CAS

Plot B.2

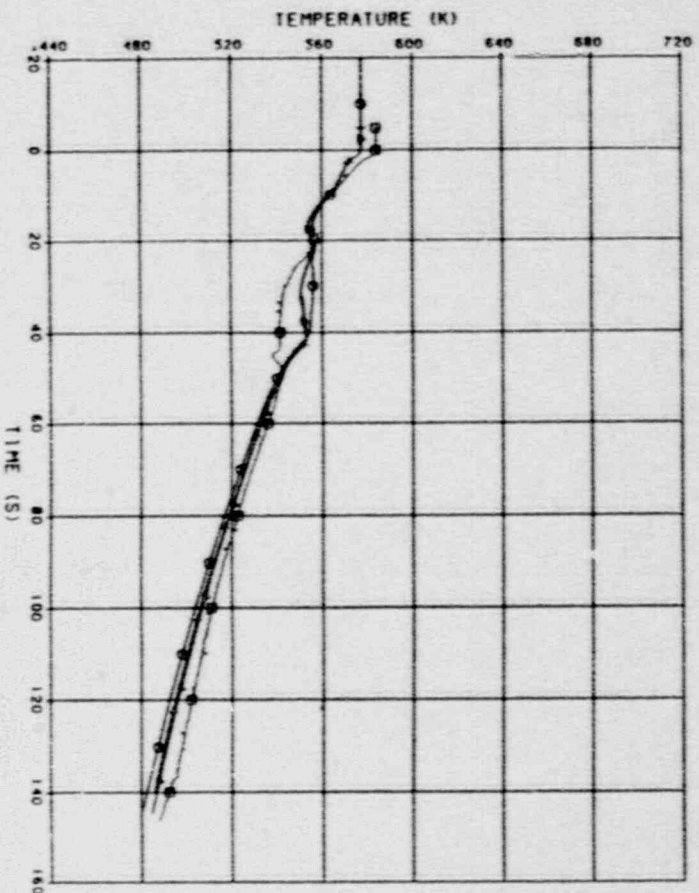




●●●●● MEAN CLAD TEMPERATURE: LEVEL 1 (119) (200 121) (244) - EXPERIMENT
 ○●●●● MEAN CLAD TEMPERATURE: LEVEL 1 (111) (111) (111) CASE A
 ▲▲▲▲ MEAN CLAD TEMPERATURE: LEVEL 1 (111) (111) (111) CASE B
 ×××× MEAN CLAD TEMPERATURE: LEVEL 1 (111) (111) (111) CASE C

Plot B.4

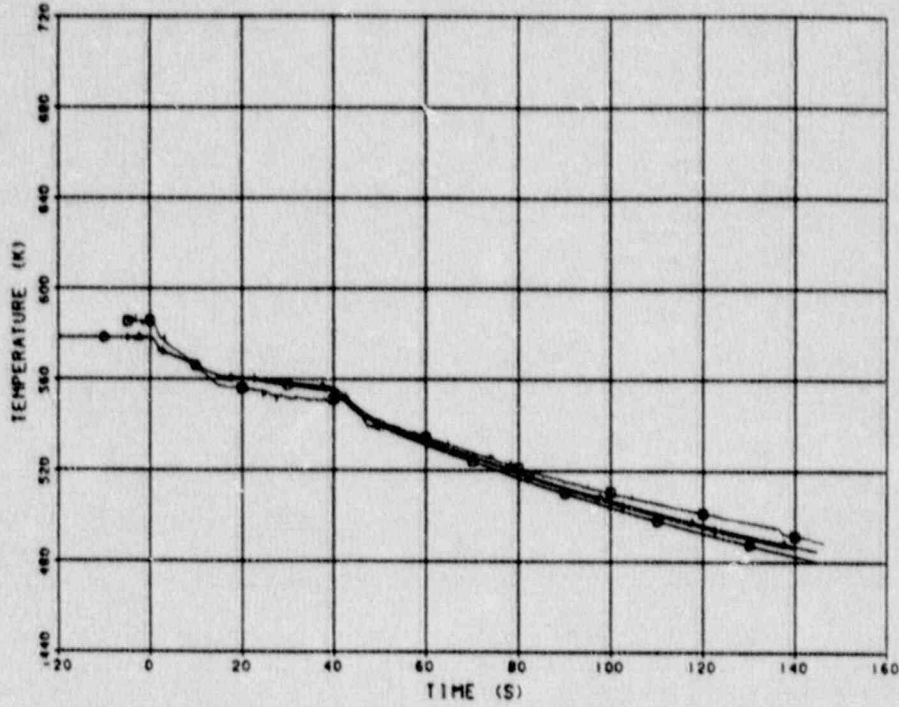
RELAP5/MOD2 CALCULATION FOR FIX-11. EXP 3051



RELAP5/MOD2 CALCULATION FOR FIX-11, EXP 3051

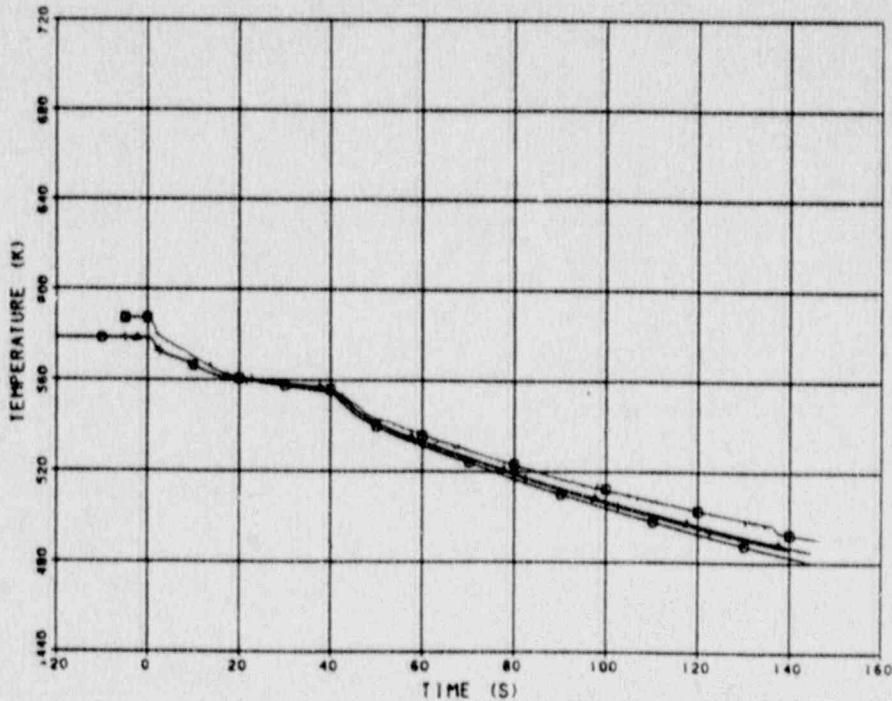
+ 9-00 REAR CLAD TEM. LEVEL 3 (T108 T183 T243 T248) - EXPERIMENT
 REAR CLAD TEM. LEVEL 3 (INITIAL 4 3000105) CASE A
 REAR CLAD TEM. LEVEL 3 (INITIAL 403000105) CASE B
 REAR CLAD TEM. LEVEL 3 (INITIAL 403000105) CASE C

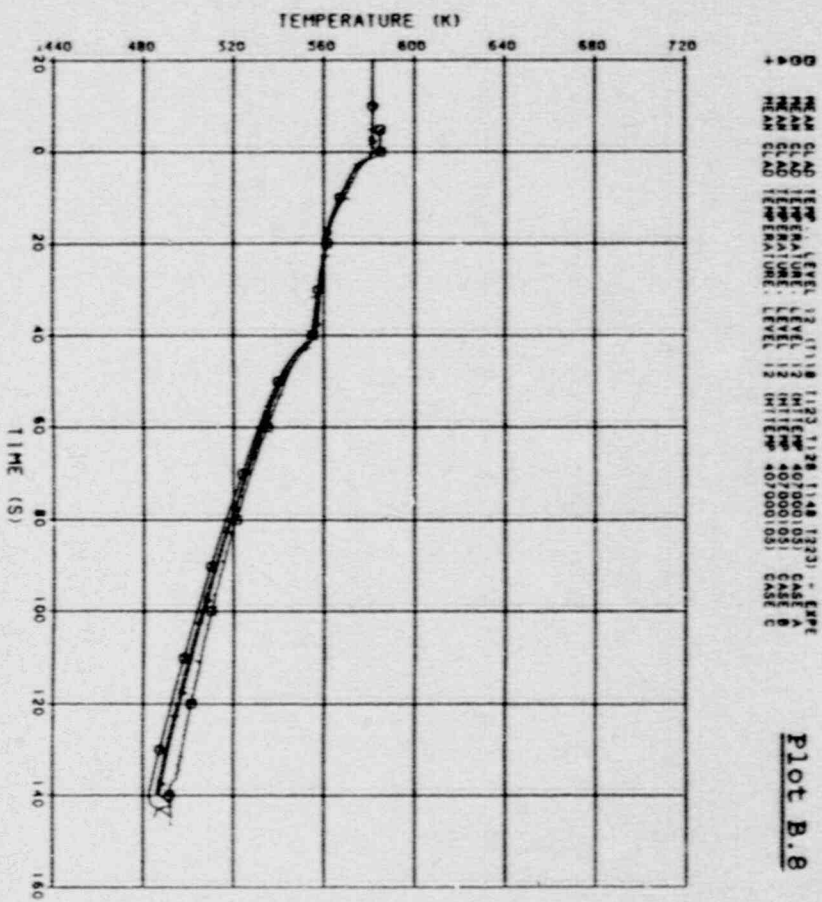
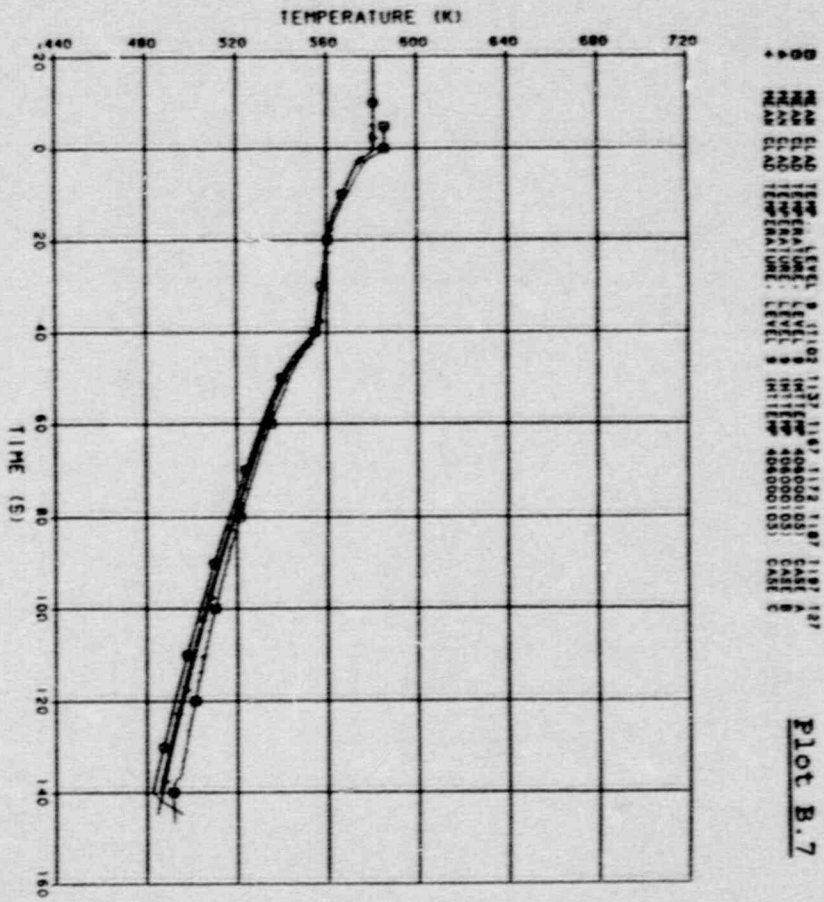
Plot B.5



+ 9-00 REAR CLAD TEM. LEVEL 5 (T202 T227 T232 T237 T252) - EXPERIMENT
 REAR CLAD TEM. LEVEL 5 (INITIAL 404000105) CASE A
 REAR CLAD TEM. LEVEL 5 (INITIAL 404000105) CASE B
 REAR CLAD TEM. LEVEL 5 (INITIAL 404000105) CASE C

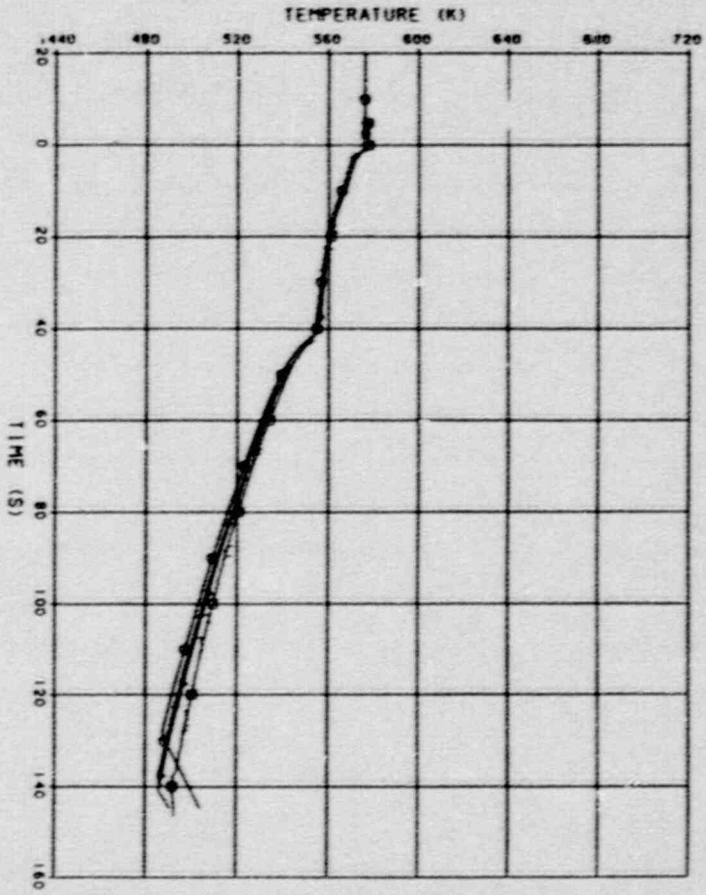
Plot B.6





RELAP5/MOD2 CALCULATION FOR FIX-11. EXP 3051

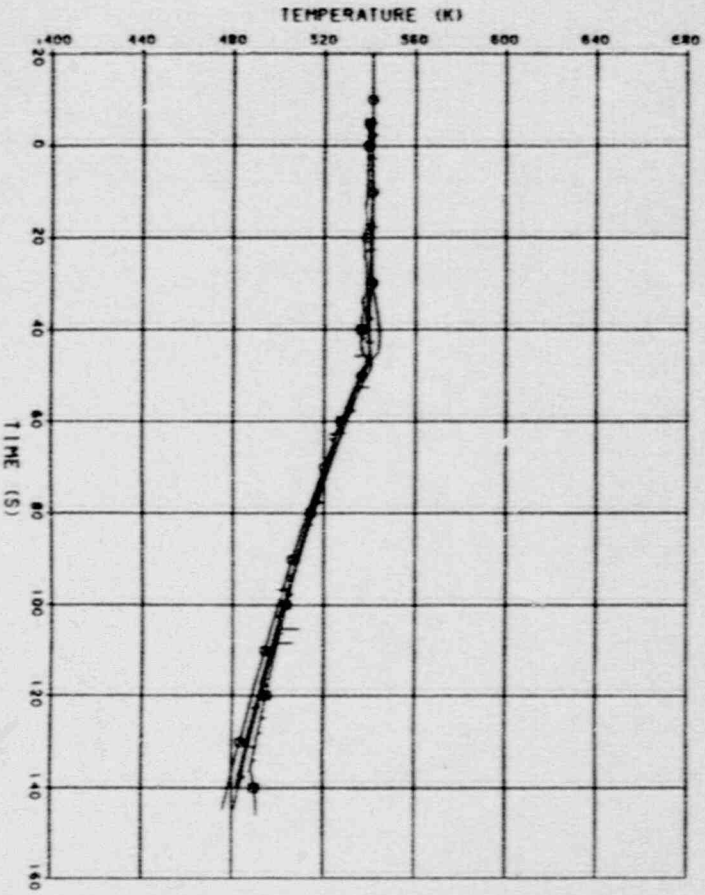
0000
+ + +
TIME (S) 20 0 20 40 60 80 100 120 140 160
TEMP (K) 400 440 480 520 560 600 640 680
LEVEL 15 (TEMP 1100 1275) - EXPERIMENT
LEVEL 15 (TEMP 410000103) CASE A
LEVEL 15 (TEMP 410000103) CASE B
LEVEL 15 (TEMP 410000103) CASE C



Plot B.9

RELAP5/MOD2 CALCULATION FOR FIX-11, EXP 3051

0000
+ + +
TIME (S) 20 0 20 40 60 80 100 120 140 160
TEMP (K) 400 440 480 520 560 600 640 680
LEVEL 15 (TEMP 1100 1275) - EXPERIMENT
LEVEL 15 (TEMP 410000103) CASE A
LEVEL 15 (TEMP 410000103) CASE B
LEVEL 15 (TEMP 410000103) CASE C

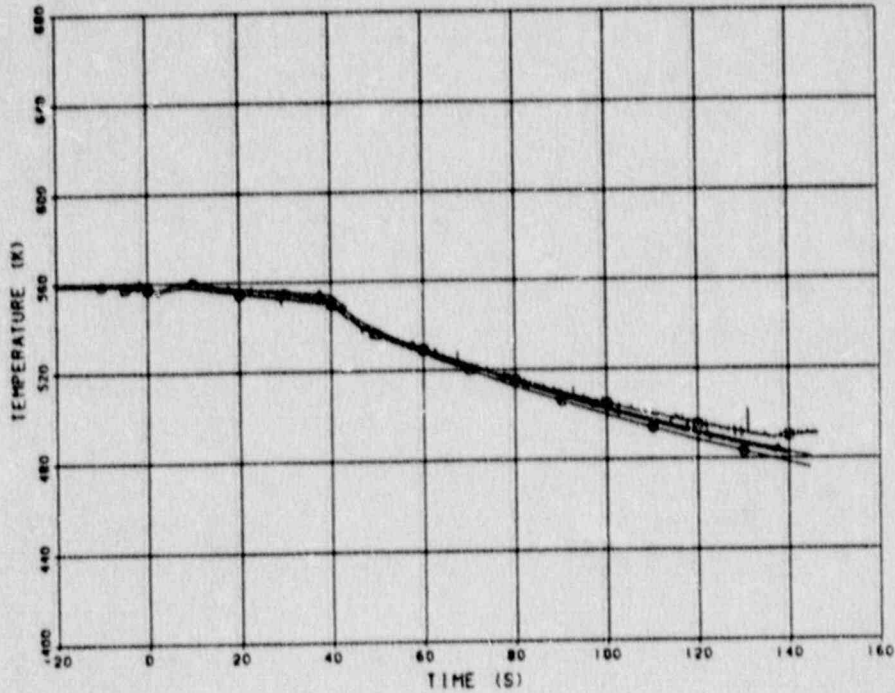


Plot B.10

RELAPS/MOD2 CALCULATION FOR FIX-11, EXP 3051

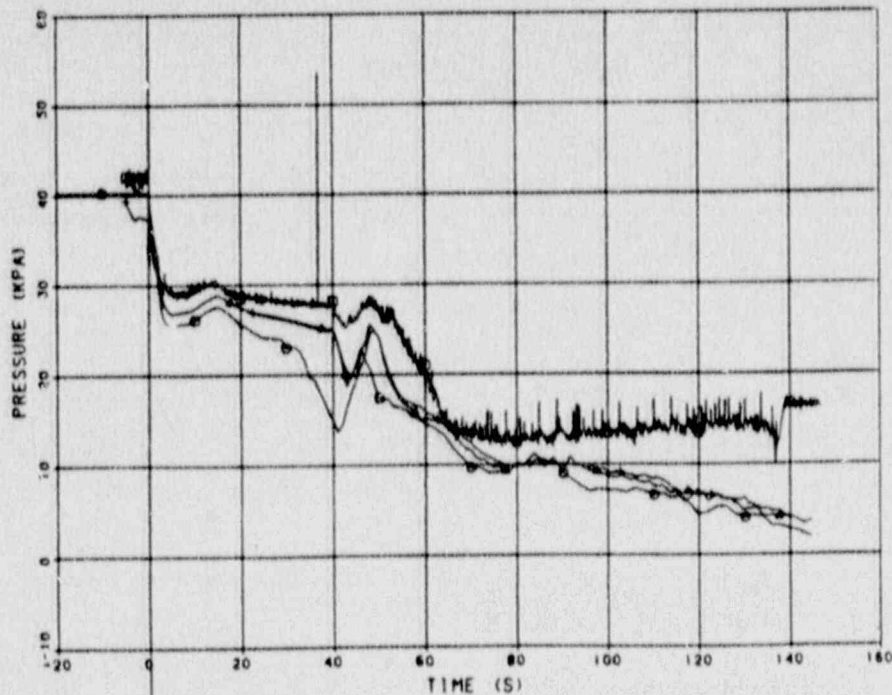
* 4-08 FLUID TEMPERATURE, CORE OUTLET (TE 14) - EXPERIMENT
 FLUID TEMPERATURE, CORE OUTLET (TEMPF 5101) CASE A
 FLUID TEMPERATURE, CORE OUTLET (TEMPF 5101) CASE B
 FLUID TEMPERATURE, CORE OUTLET (TEMPF 5101) CASE C

Plot B.11



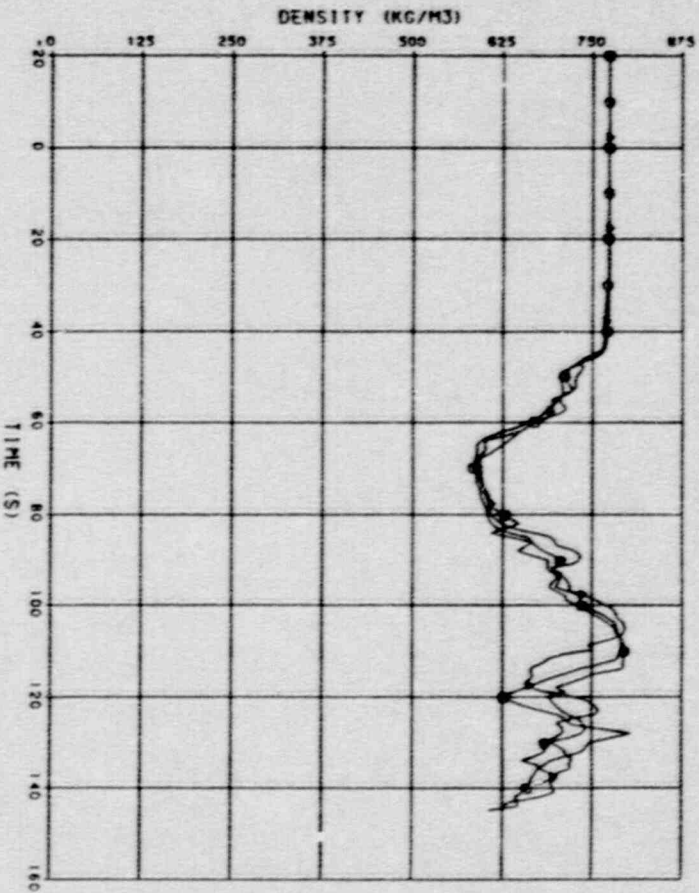
* 4-09 DIFF. PRESSURE, CORE (DPT 5 - DPT 6 + DPT 12) - EXPE
 DIFF. PRESSURE, CORE (FROM P 401 - P 5101) CASE A
 DIFF. PRESSURE, CORE (FROM P 401 - P 5101) CASE B
 DIFF. PRESSURE, CORE (FROM P 401 - P 5101) CASE C

Plot B.12



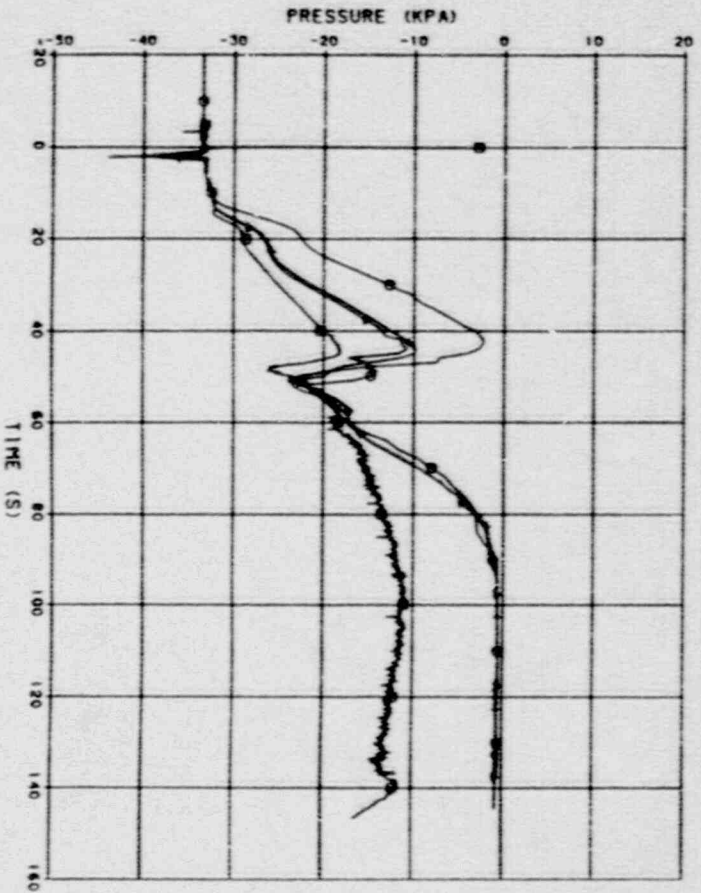
00 FLUID DENSITY VESSEL BOTTOM (RHO 3101) CASE A
 01 FLUID DENSITY VESSEL BOTTOM (RHO 3101) CASE B
 02 FLUID DENSITY VESSEL BOTTOM (RHO 3101) CASE C

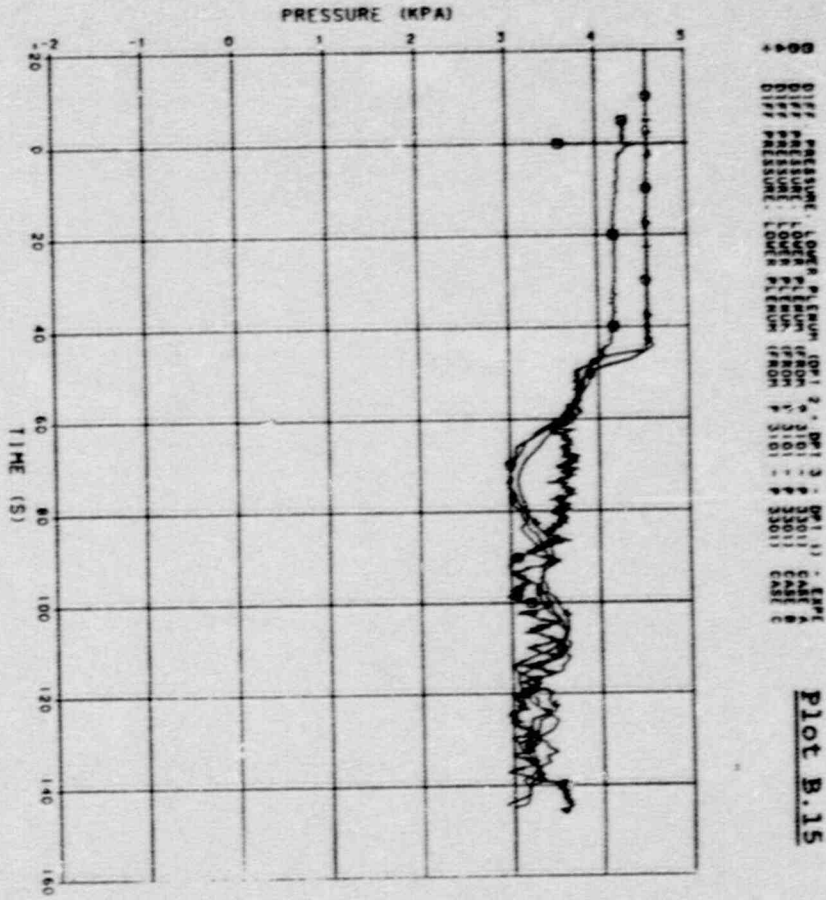
Plot B.13



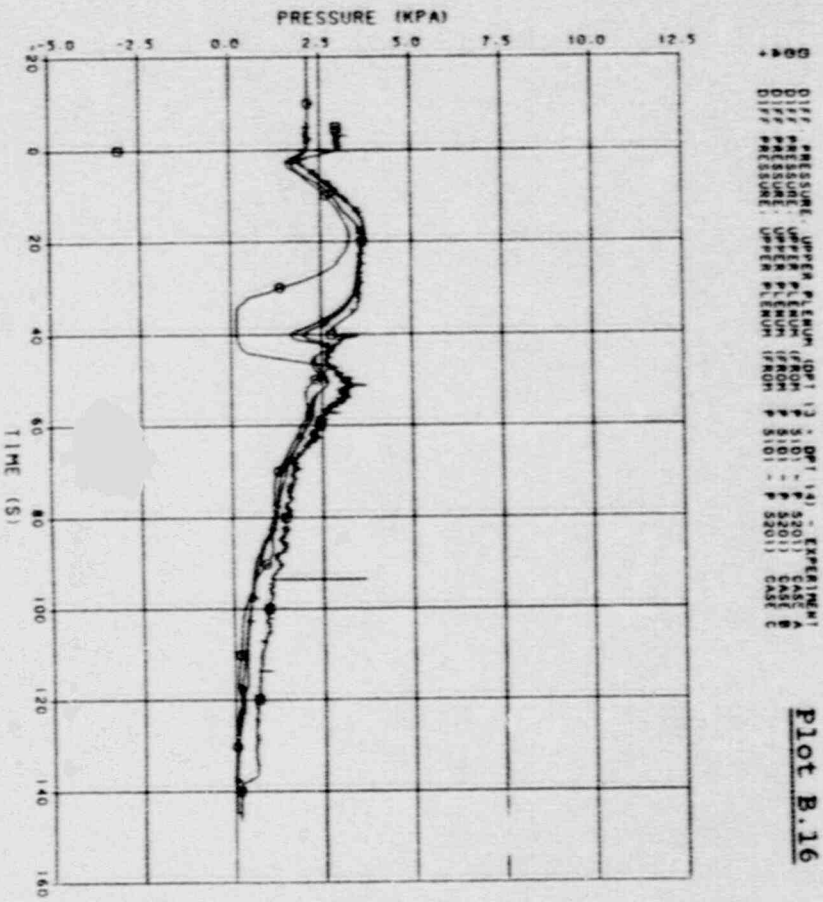
00 DIFF. PRESSURE DOWNCOMER (DP1 37 7103 - P 7201) CASE A
 01 DIFF. PRESSURE DOWNCOMER (FROM P 7103 - P 7201) CASE B
 02 DIFF. PRESSURE DOWNCOMER (FROM P 7103 - P 7201) CASE C

Plot B.14





RELAP5/MOD2 CALCULATION FOR FIX-II, EXP 3051

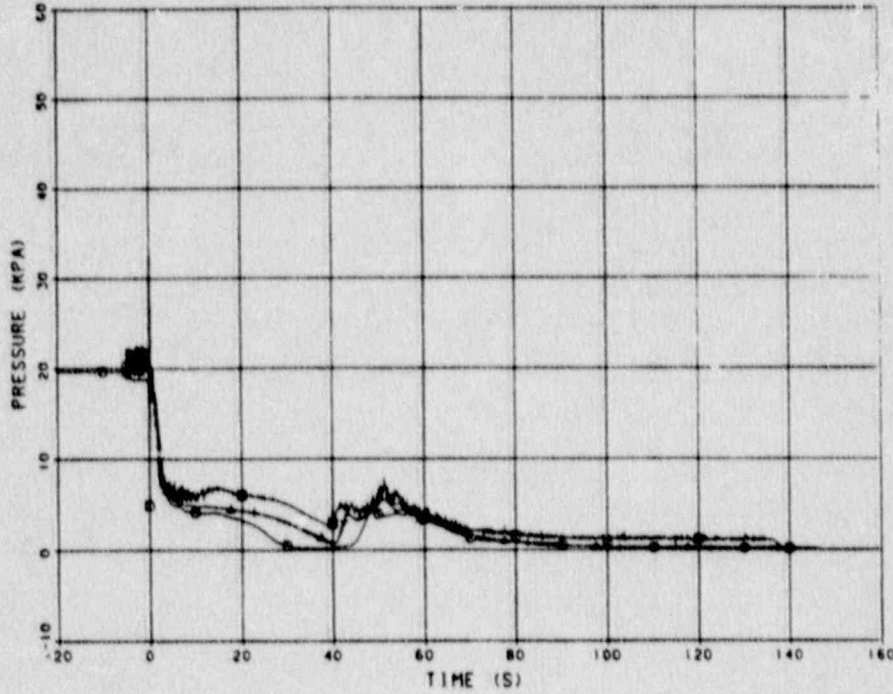


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RELAP5/MOD2 CALCULATION FOR FIX-11. EXP 3051

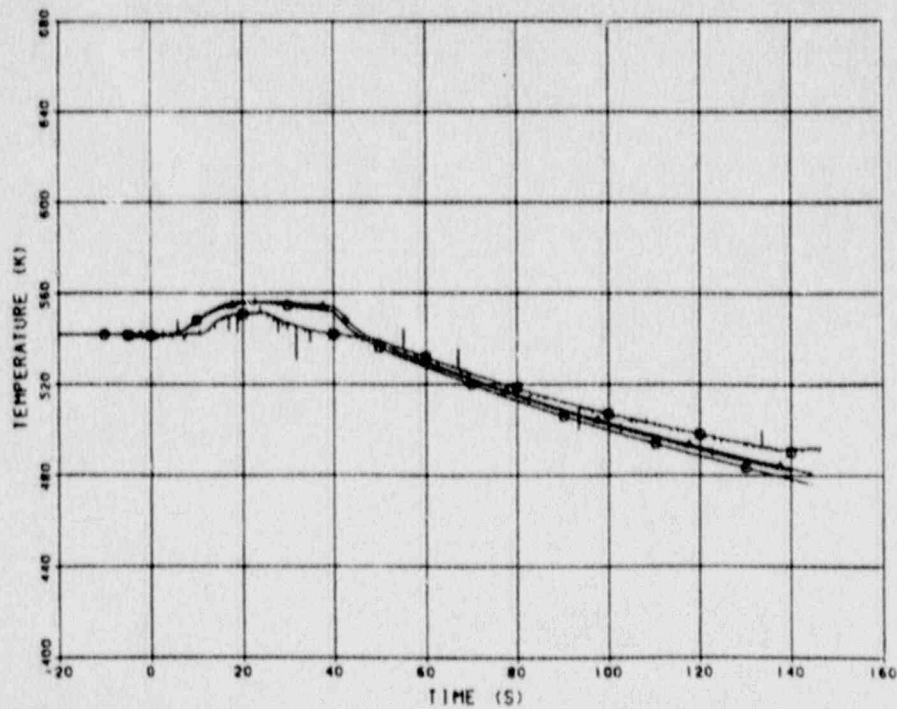
1) DIFF. PRESSURE, STEAM SEPARATOR DRIFICE (DP1 S6) - EXPERIME
2) DIFF. PRESSURE, STEAM SEPARATOR DRIFICE (P S201 - P S202) C
3) DIFF. PRESSURE, STEAM SEPARATOR DRIFICE (P S201 - P S202) C
4) DIFF. PRESSURE, STEAM SEPARATOR DRIFICE (P S201 - P S202) C

Plot B.17



1) FLUID TEMPERATURE, DOWNCOMER BOTTOM (TEMP 7108) CASE A
2) FLUID TEMPERATURE, DOWNCOMER BOTTOM (TEMP 7108) CASE B
3) FLUID TEMPERATURE, DOWNCOMER BOTTOM (TEMP 7108) CASE C
4) FLUID TEMPERATURE, DOWNCOMER BOTTOM (TEMP 7108) CASE C

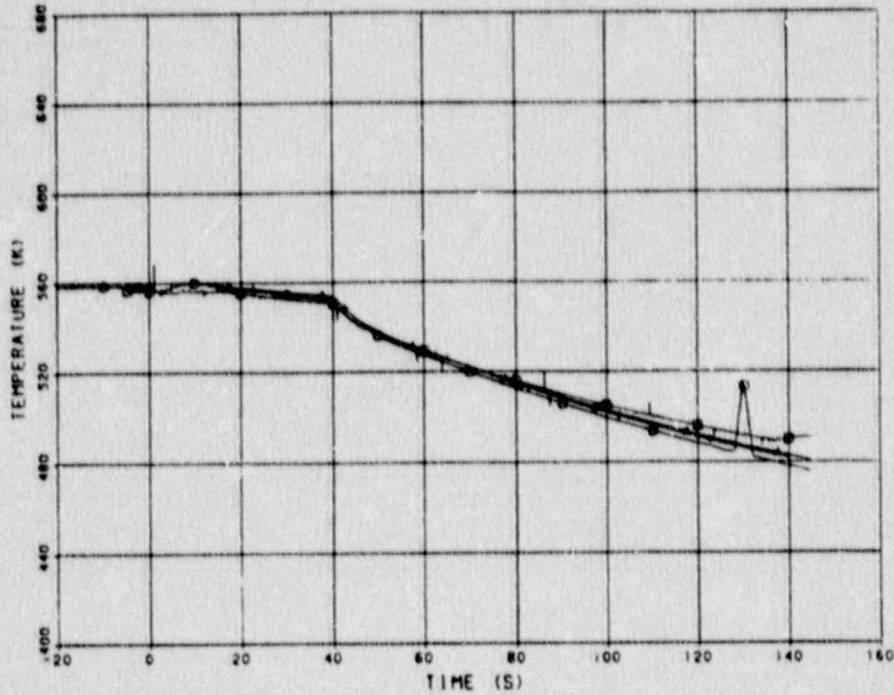
Plot B.18



RELAP5/MOD2 CALCULATION FOR FIX-II. EXP 3051

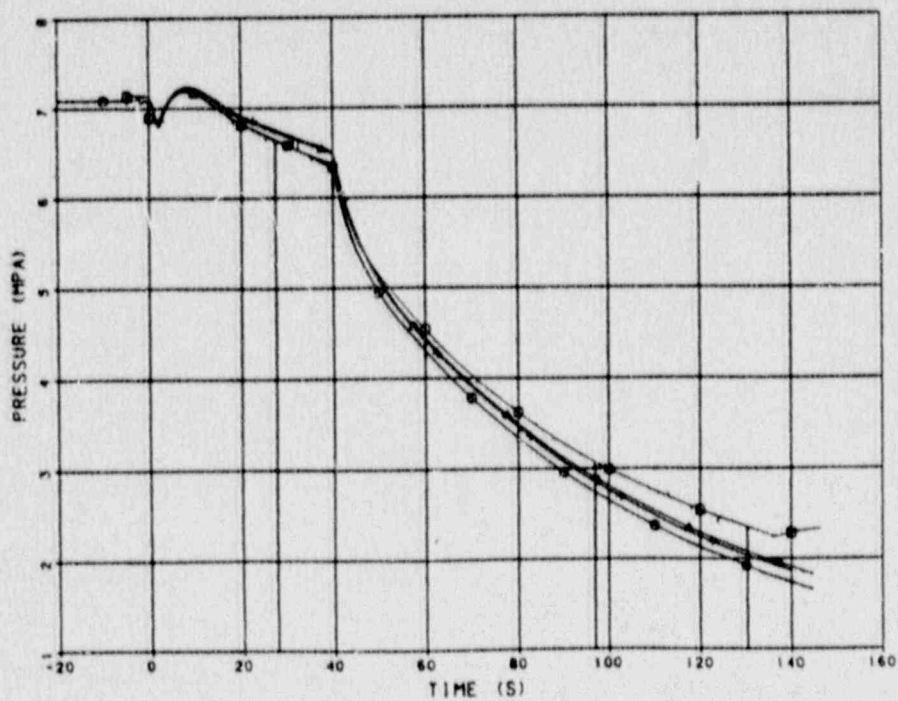
+ 9.00 FLUID TEMPERATURE, UPPER PLENUM (TE 15) - EXPERIMENT
 FLUID TEMPERATURE, UPPER PLENUM (TEMPF 5201) CASE A
 FLUID TEMPERATURE, UPPER PLENUM (TEMPF 5201) CASE B
 FLUID TEMPERATURE, UPPER PLENUM (TEMPF 5201) CASE C

Plot B.19



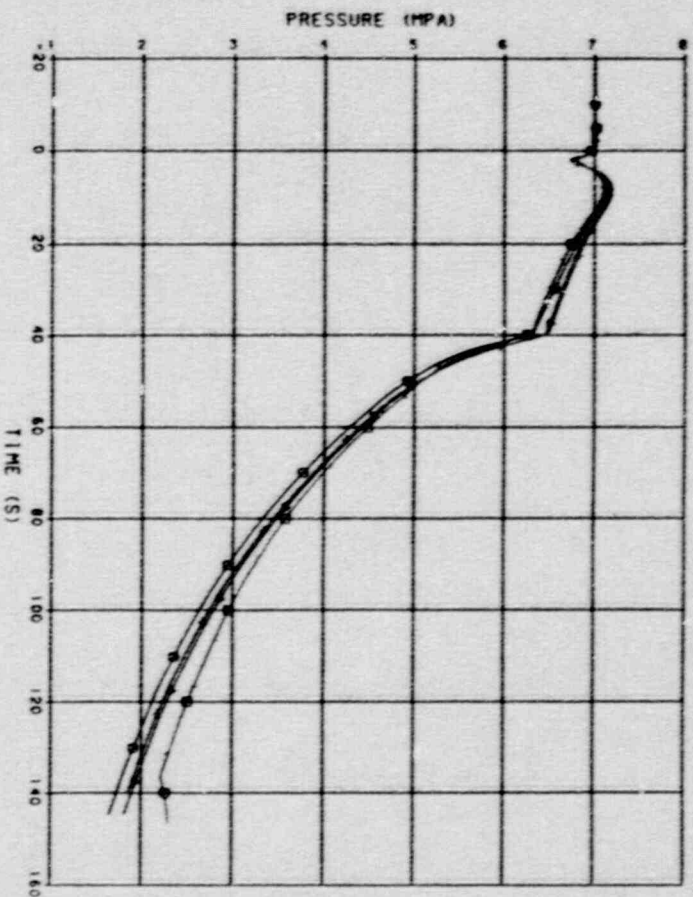
+ 9.00 PRESSURE, LOWER PLENUM (PT 3) - EXPERIMENT
 PRESSURE, LOWER PLENUM (P 3101) CASE A
 PRESSURE, LOWER PLENUM (P 3101) CASE B
 PRESSURE, LOWER PLENUM (P 3101) CASE C

Plot B.20



0 0
 + + PRESSURE: UPPER PLENUM (P 1 4) EXPERIMENT
 PRESSURE: UPPER PLENUM (P 520) CASE A
 PRESSURE: UPPER PLENUM (P 520) CASE B
 PRESSURE: UPPER PLENUM (P 520) CASE C

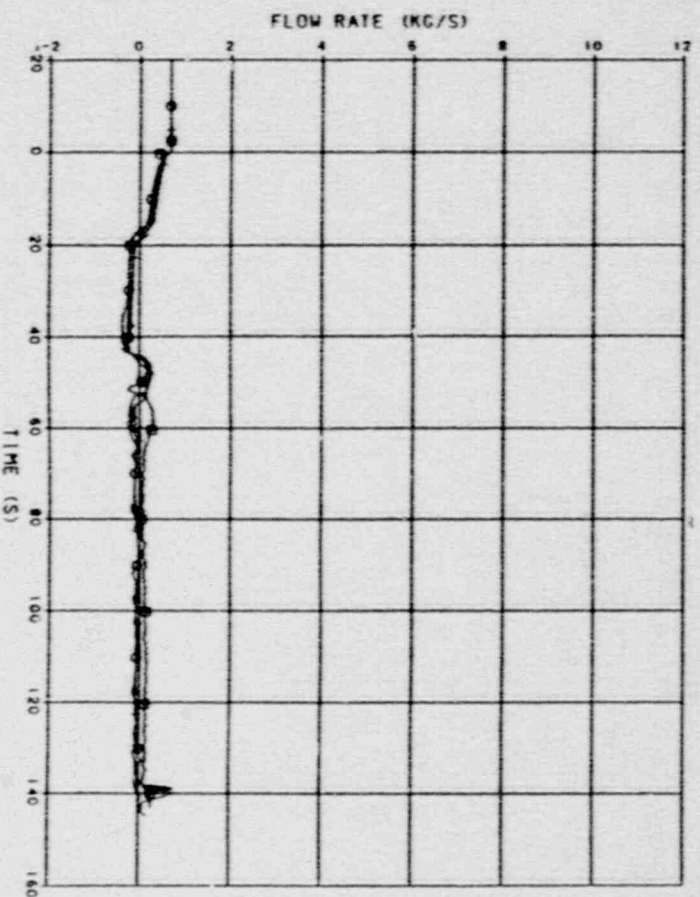
Plot B.21



0 0
 + + MASS FLOW RATE: BYPASS - EXPERIMENT
 MASS FLOW RATE: BYPASS (MFLD) 117 CASE A
 MASS FLOW RATE: BYPASS (MFLD) 117 CASE B
 MASS FLOW RATE: BYPASS (MFLD) 117 CASE C

Plot B.22

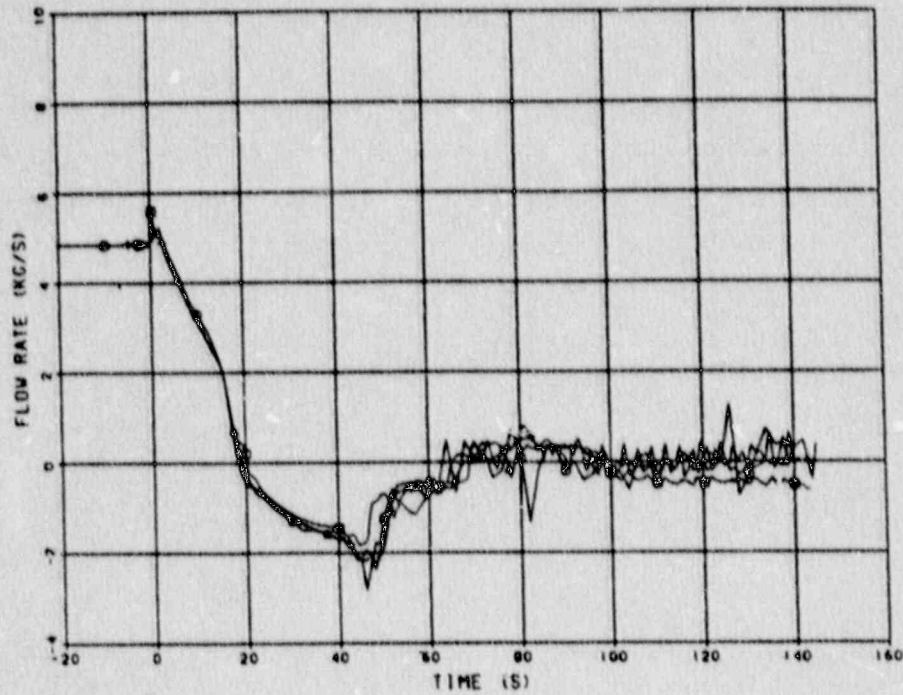
RELAP5/MOD2 CALCULATION FOR FIX-11. EXP 3051



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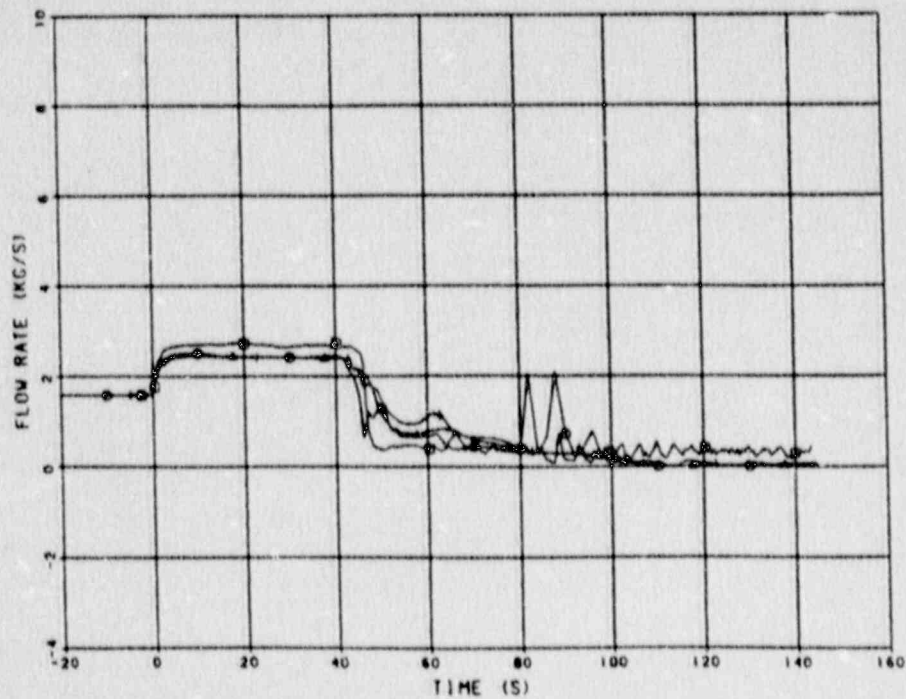
4.008 MASS FLOW RATE, I.L., PUMP - EXPERIMENT CASE A
 MASS FLOW RATE, I.L., PUMP (NO.FLOW.J.20102) CASE B
 4.009 MASS FLOW RATE, I.L., PUMP (NO.FLOW.J.20102) CASE B
 MASS FLOW RATE, I.L., PUMP (NO.FLOW.J.20102) CASE C

Plot B.23



4.808 MASS FLOW RATE, B.L., PUMP - EXPERIMENT CASE A
 MASS FLOW RATE, B.L., PUMP (NO.FLOW.J.20202) CASE B
 4.809 MASS FLOW RATE, B.L., PUMP (NO.FLOW.J.20202) CASE B
 MASS FLOW RATE, B.L., PUMP (NO.FLOW.J.20202) CASE C

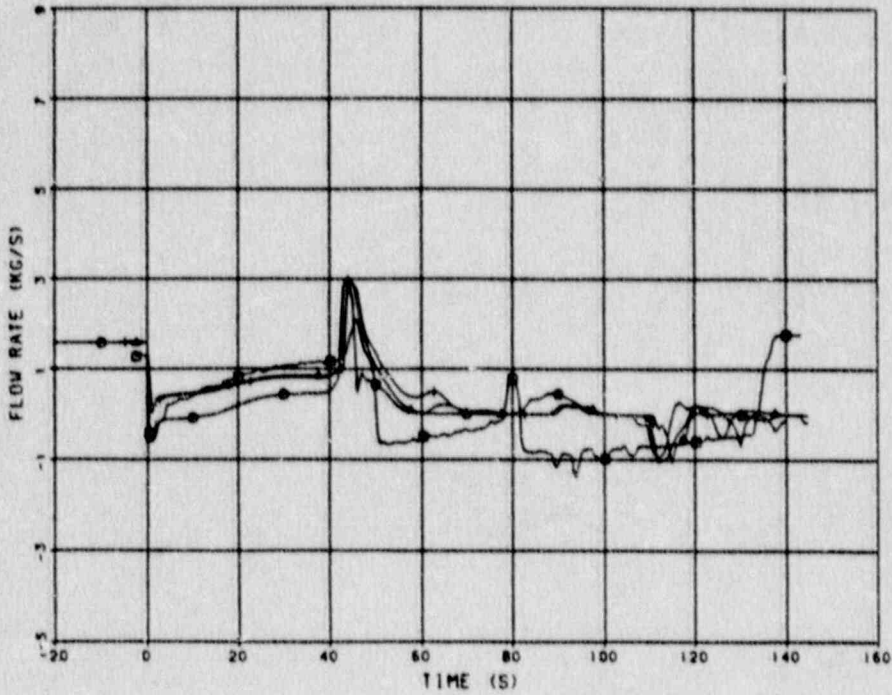
Plot B.24



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● MASS FLOW RATE, B.L. VESSEL INLET (SPOOL PIECE K10) - EXPER
○ MASS FLOW RATE, B.L. VESSEL INLET (INFLOWJ 9702) CASE A
+ MASS FLOW RATE, B.L. VESSEL INLET (INFLOWJ 9702) CASE B
* MASS FLOW RATE, B.L. VESSEL INLET (INFLOWJ 9702) CASE C

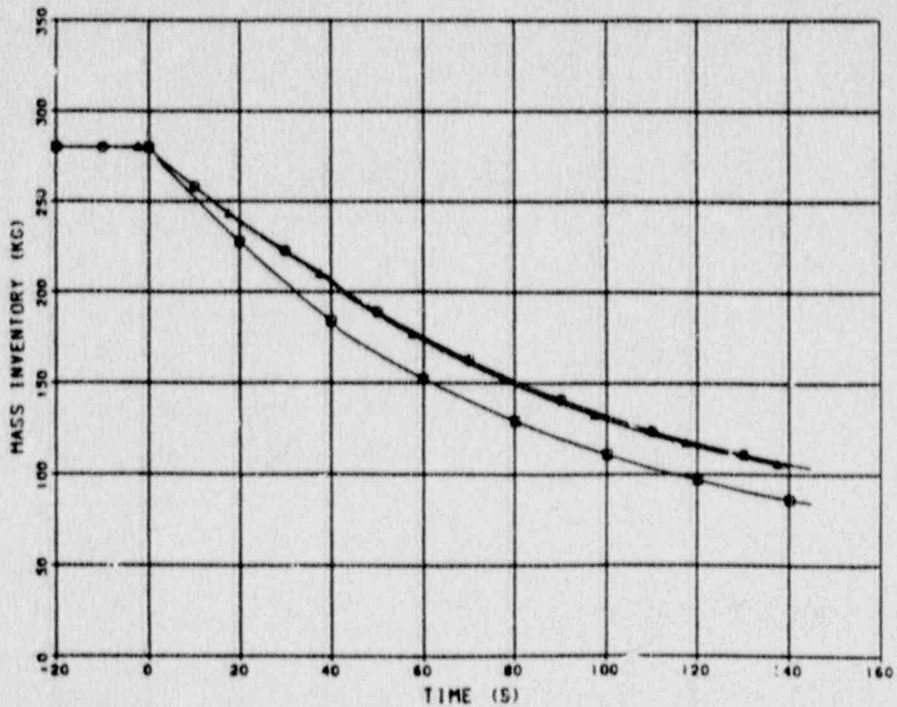
Plot B.25



RELAP5/MOD2 CALCULATION FOR FIX-11. EXP 3051

●●● TOTAL MASS. IN SYSTEM CASE A
○ TOTAL MASS. IN SYSTEM CASE B
* TOTAL MASS. IN SYSTEM CASE C

Plot B.26

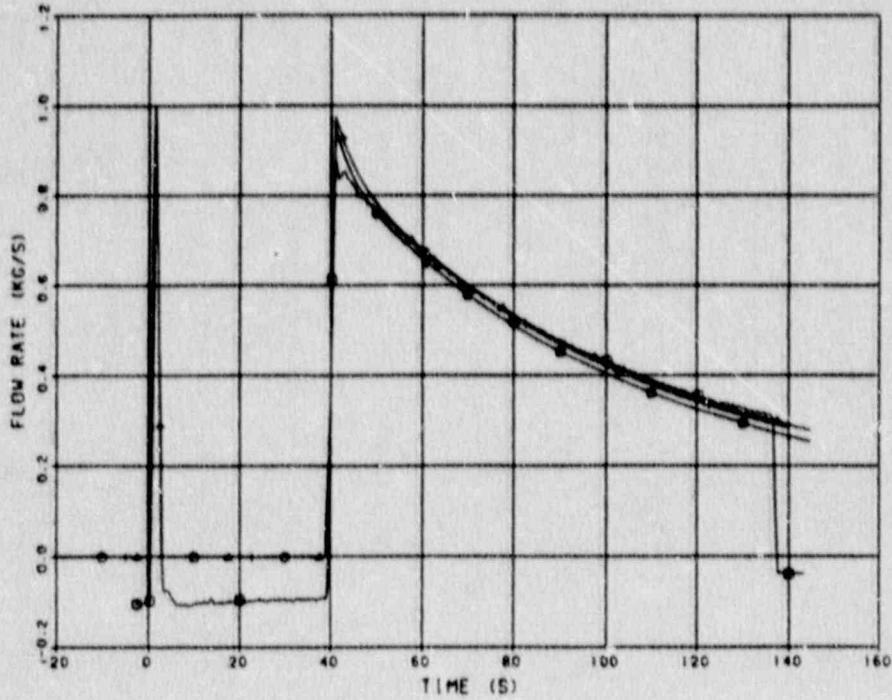


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RELAP5/MOD2 CALCULATION FOR FIX-11. EXP 3051

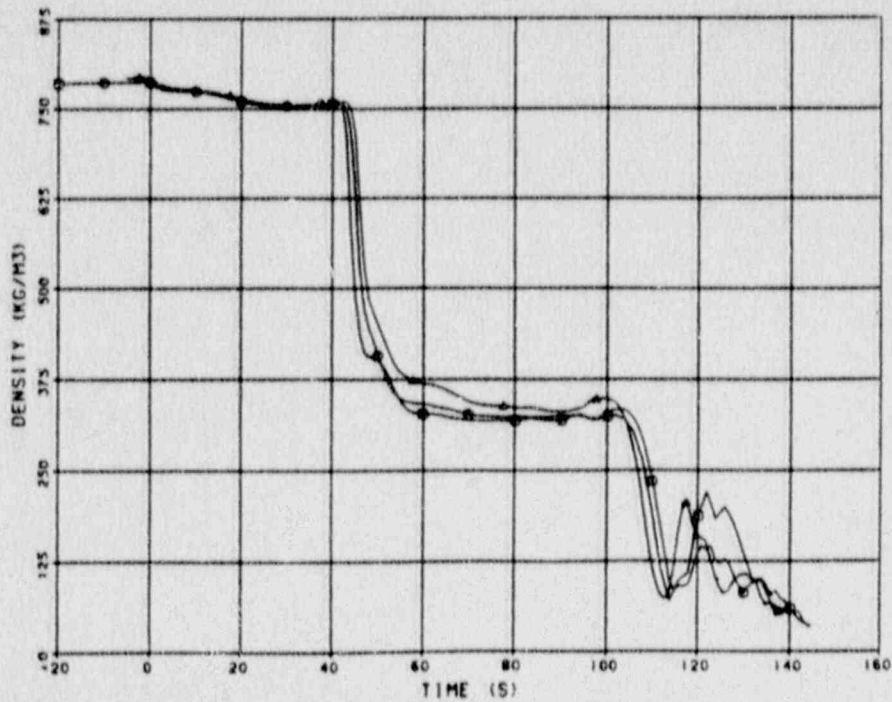
4-908 MASS FLOW RATE STEAM RELIEF - EXPERIMENT CASE A
 MASS FLOW RATE STEAM RELIEF (RFLOWJ 404) CASE B
 MASS FLOW RATE STEAM RELIEF (RFLOWJ 404) CASE C

Plot B.27



4-008 FLUID DENSITY: BREAK (RHO 8601) CASE A
 FLUID DENSITY: BREAK (RHO 8601) CASE B
 FLUID DENSITY: BREAK (RHO 8601) CASE C

Plot B.28

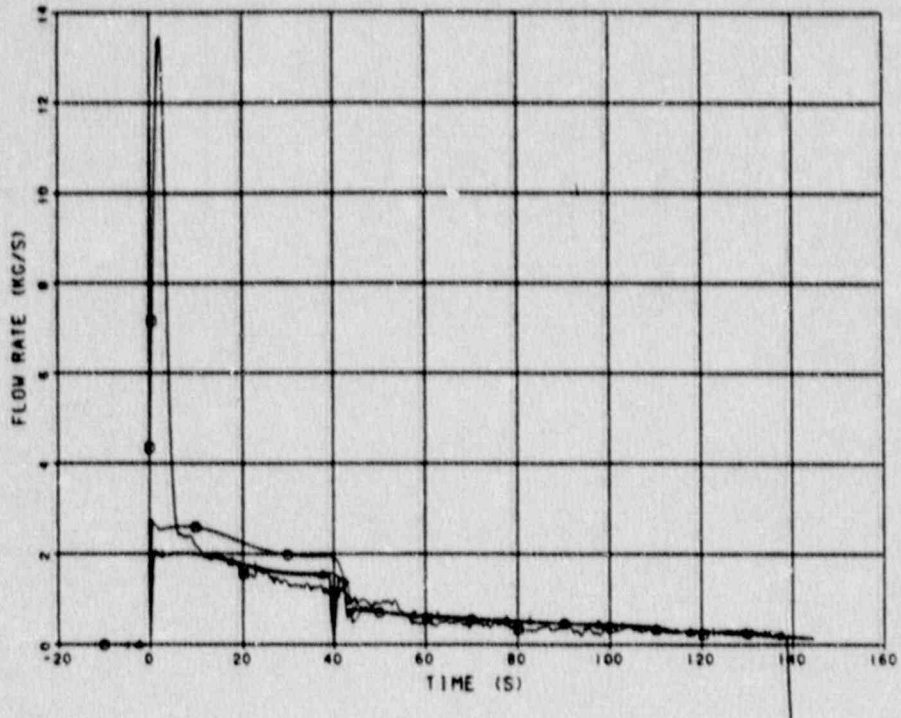


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RELAP5/MOD2 CALCULATION FOR FIX-11. EXP 3051

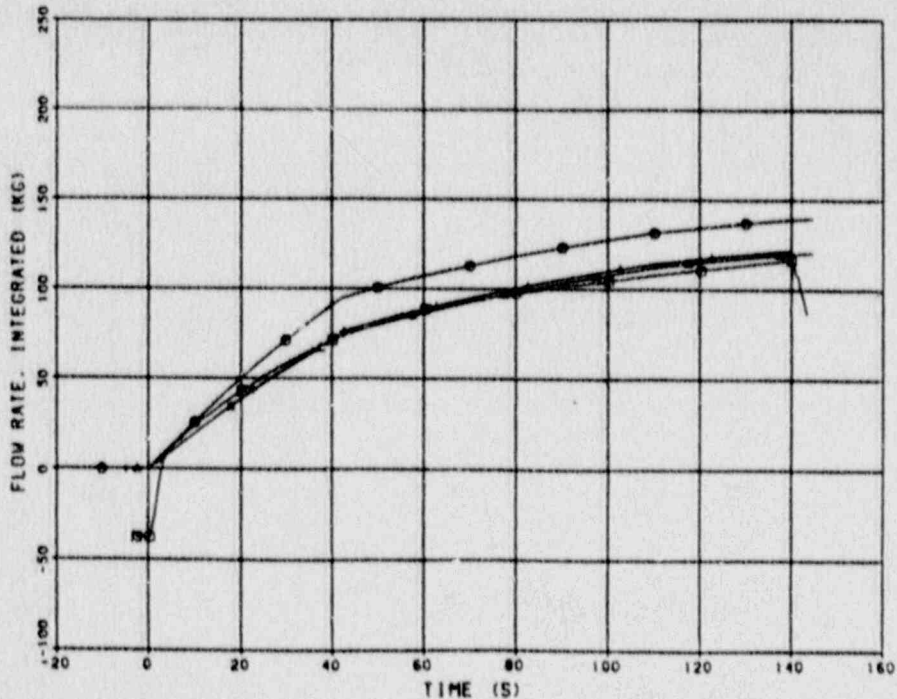
+ 000 MASS FLOW RATE. BREAK FROM T2 INVENTORY - EXPERIMENT
+ 000 MASS FLOW RATE. BREAK (INFLOW 182) CASE A
+ 000 MASS FLOW RATE. BREAK (INFLOW 182) CASE B
+ 000 MASS FLOW RATE. BREAK (INFLOW 182) CASE C

Plot B.29



+ 000 MASS LOSS. BREAK FLOW RECEIVER - EXPERIMENT
+ 000 BREAK TOTAL MASS LOSS (CNTRLVAR 55) CASE A
+ 000 BREAK TOTAL MASS LOSS (CNTRLVAR 55) CASE B
+ 000 BREAK TOTAL MASS LOSS (CNTRLVAR 55) CASE C

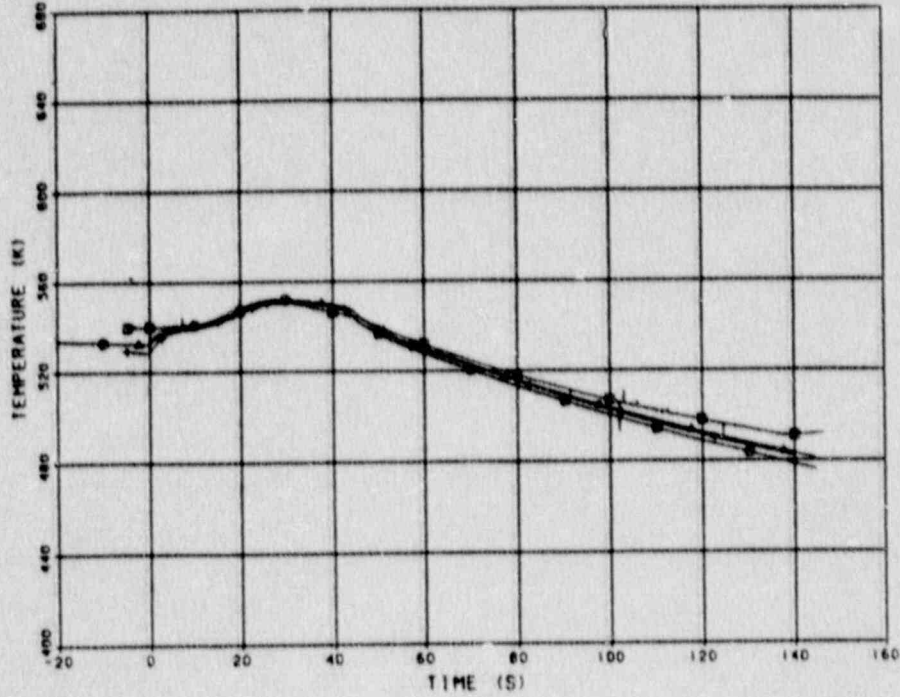
Plot B.30



RELAP5/MOD2 CALCULATION FOR FIX-11. EXP 3051

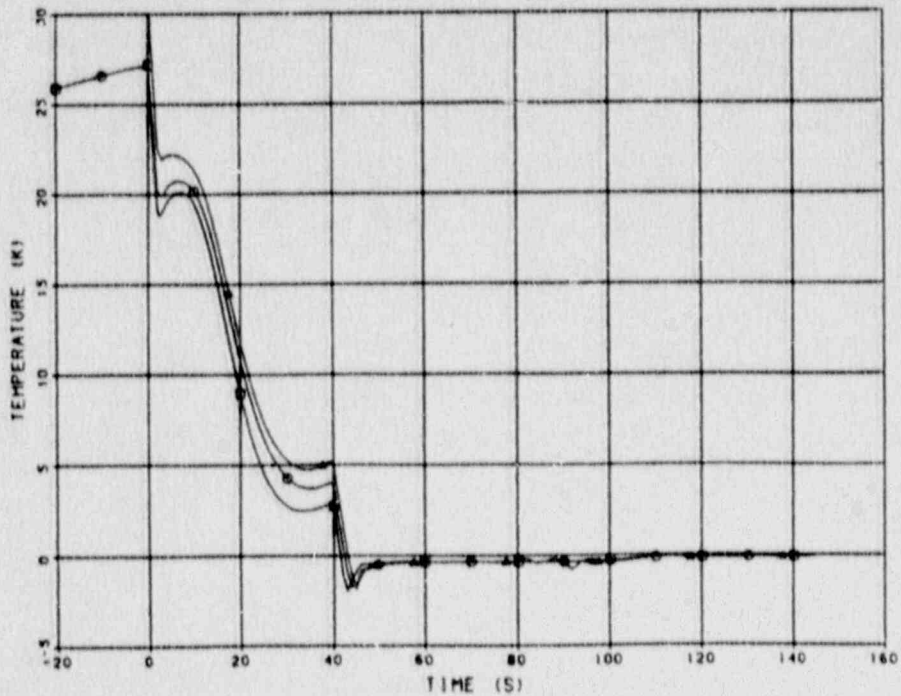
* 9 0 0 FLUID TEMPERATURE, BREAK INLET (TE 34) - EXPERIMENT
FLUID TEMPERATURE, BREAK INLET (TEMP 9601) CASE A
FLUID TEMPERATURE, BREAK INLET (TEMP 9601) CASE B
FLUID TEMPERATURE, BREAK INLET (TEMP 9601) CASE C

Plot B.31



* 0 0 SUBCOOLING, BREAK INLET (TEMP 9101 - TEMP 9101) CASE A
SUBCOOLING, BREAK INLET (TEMP 9101 - TEMP 9101) CASE B
SUBCOOLING, BREAK INLET (TEMP 9101 - TEMP 9101) CASE C

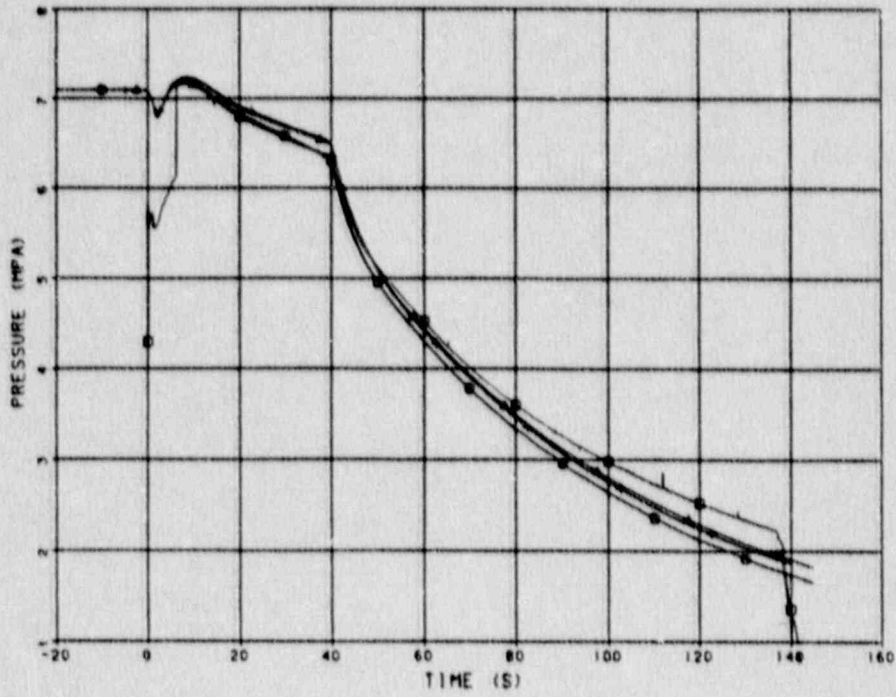
Plot B.32



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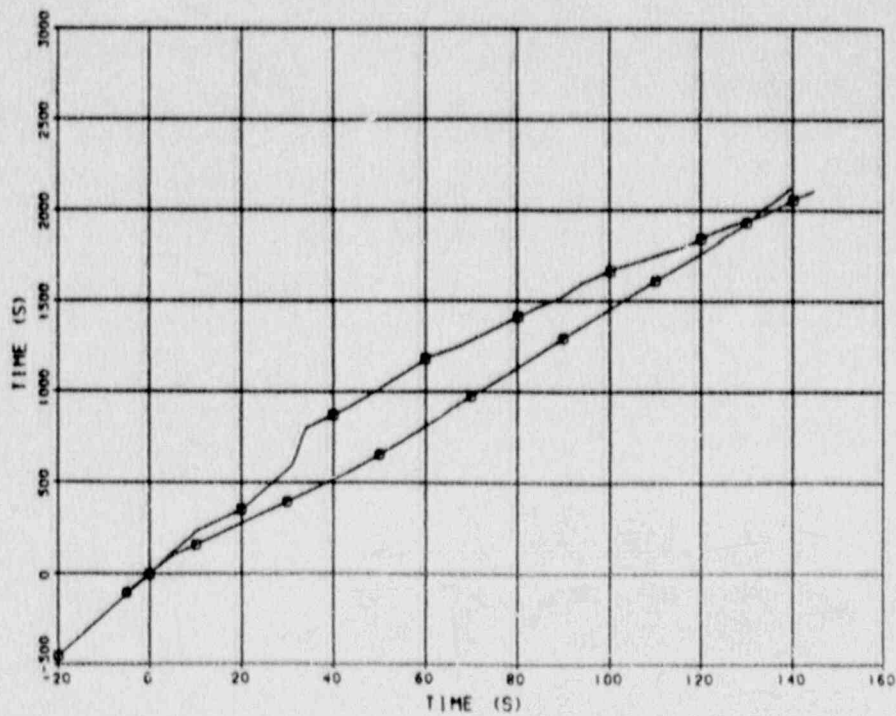
OB PRESSURE BREAK INLET IP1 61 - EXPERIMENT
A PRESSURE BREAK INLET IP 06011 CASE A
+ PRESSURE BREAK INLET IP 06011 CASE B
+ PRESSURE BREAK INLET IP 06011 CASE C

Plot B.33



OB CPU TIME CASE A
CPU TIME CASE C

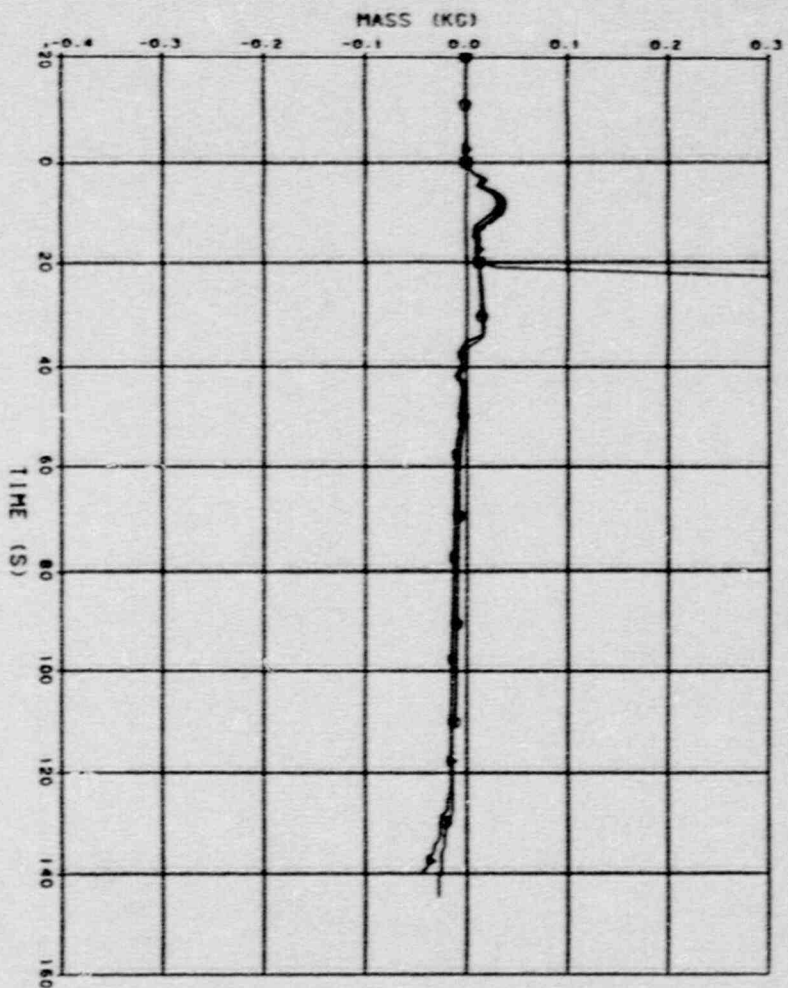
Plot B.34



RELAP5/MOD2 CALCULATION FOR FIX-11. EXP 3051

0 MASS ERROR CASE 1
1 MASS ERROR CASE 2
2 MASS ERROR CASE 3

Plot B.35



1986-09-17

Calculation to experiment data uncertainties

Case A

 CALCULATION-TO-EXPERIMENT DATA UNCERTAINTY ANALYSIS FOR NRC/ICAP

FIRST LINE : DIFFERENCE BETWEEN CALCULATED AND (AVERAGED) EXPERIMENTAL DATA AT END OF THE INTERVAL
 SECOND LINE : MEAN DIFFERENCE OVER THE INTERVAL
 THIRD LINE : MEAN SIGMA OVER THE INTERVAL (ROOT MEAN SQUARE OF THE DIFFERENCE)

- CODES -		- - - - TIME INTERVAL - - - -							
CALC.	EXP.	0.0 - 6.000	- 12.00	- 20.00	- 30.00	- 45.00	- 65.00	- 85.00	- 135.0
P 1A - P 3		-.100E-01 -.642E-01 .876E-01	-.120E-02 -.208E-02 .786E-02	-.172E-01 -.645E-02 .780E-02	-.133E-01 -.109E-01 .263E-01	-.119 -.288E-01 .493E-01	-.227 -.188 .201	-.333 -.274 .278	-.448 -.374 .407
P 2A - P 4		-.285E-01 -.346E-02 .360E-01	-.453E-01 -.422E-01 .428E-01	-.861E-01 -.466E-01 .667E-01	-.678E-01 -.339E-01 .861E-01	-.857E-01 -.138E-01 .423E-01	-.205 -.166 .170	-.304 -.249 .280	-.420 -.265 .267
P 3A - P 6		1.02 1.27 1.58	-.281E-01 -.722E-01 .206	-.887E-01 -.318E-01 .278E-01	-.388E-01 -.372E-01 .273E-01	-.101 -.686E-02 .283E-01	-.207 -.178 .179	-.205 -.257 .258	-.433 -.378 .380
PD4A - D 4		-.898 1.01 4.64	-.241 -.722 .777	1.88 -.611 .847	1.73 1.74 1.73	1.33 1.74 1.77	1.86 2.23 2.88	-.183 -.492 .642	.745E-02 .270 .320
PD1A - D LP		.315 .282 .289	.336 .330 .330	.348 .357 .357	.345 .355 .355	.484 .378 .378	-.488 -.130E-01 -.167	-.163E-01 -.414 .462	.188E-01 .154 .233
PDCA - D CO		-3.22 -1.85 2.82	-2.86 -3.33 3.34	-2.93 -2.89 2.81	-5.02 -4.01 4.04	-7.29 -8.59 8.98	+1.48 -6.80 7.02	-6.01 -2.84 3.60	-10.2 -8.14 8.29
PVDA - D UP		-.352 -.464 .491	-.418 -.421 .426	-.343 -.463 .466	-2.08 -.853 .985	-1.66 -2.78 2.80	-.423 -.864 .734	-.801 -.387 .396	-.859 -.885 .890
PDDA - D DC		-.300E-02 -.423 1.18	.159 -.888E-01 .139	6.25 4.06 4.52	12.0 8.76 8.92	14.8 18.0 15.1	3.62 4.31 6.68	10.5 9.14 9.33	15.1 11.6 11.8
PDSA - D S6		-.926 -.488 1.97	-2.27 -1.72 1.75	-2.72 -2.61 2.67	-4.57 -3.73 3.79	-3.86 -3.69 3.78	-.627 -1.29 1.60	-.880 -.852 .867	-.898 -.921 .927
MF1A - X602		-.108 -.473E-01 -.792E-01	-.881E-01 -.110 -.110	-.432E-01 -.784E-01 -.102	-.192E-02 -.108E-01 -.188E-01	-.923E-01 -.787E-01 -.633E-01	-.186 -.196 -.318	-.215 -.182 .161	-.198 -.193 .196
MF2A - X603		-.425E-01 -.285E-01 .124	-.229 -.471E-01 .617E-01	-.785 -.141 .325	-.185 -.199 .228	-.285 -.167 .198	-.488 -.296 .580	-.806 -.240 .624	1.04 .332 .830
MF3A - X604		-.168 -.124 -.172	-.206 -.188 .188	-.297 -.263 .265	-.226 -.261 .262	-.802 -.318 .381	.116 -.234 .555	.423 .333 .586	-.211 -.228 .322
MF5A - X607		.866E-01 .112 .132	.101 .104 .104	.830E-01 .886E-01 .807E-01	.823E-01 .848E-01 .849E-01	.139E-01 .801E-01 .867E-01	-.188E-01 -.745E-02 -.126E-01	-.238E-01 -.200E-01 -.203E-01	-.370E-01 -.288E-01 -.290E-01
MF4A - X610		-.389 -.436E-02 .287	-.676 -.452 .456	-.600 -.606 .607	-.629 -.610 .611	-.628 -.311 .789	.645 .386 .762	1.10 .627 .891	-.731 .525 .646
MF6A - X636		-.233E-01 -8.86 6.87	.631 -.305 .344	.850 .835 .839	.890 .873 .878	-.286 -.272 .638	-.850E-01 -.589E-01 -.171	-.575E-01 -.102 .116	-.650E-01 -.108E-01 .641E-01
TF1A - T 3		2.42 1.82 1.86	2.26 2.26 2.28	2.78 2.82 2.84	2.45 2.77 2.81	6.60 6.14 6.38	-.280 .823 1.37	-2.80 -1.27 1.46	-7.71 -8.23 8.44
TF2A - T 14		1.43 1.36 1.41	2.81 1.88 1.91	1.85 1.71 1.73	2.20 2.14 2.20	.760 1.43 1.96	-1.44 -.738 1.01	-6.09 -2.68 2.83	-8.11 -6.61 6.76
TF4A - T 18		2.64 1.38 1.66	3.46 3.25 3.27	1.87 2.25 2.36	1.83 1.81 1.81	-.380 1.19 1.38	-1.84 -1.12 1.27	-4.89 -3.01 3.18	-8.12 -8.24 7.62
TF3A - T 31		-6.66 -.356 .660	7.13 4.18 4.92	5.48 5.93 6.01	7.85 5.70 6.80	1.10 7.81 8.20	-4.21 -3.06 3.33	-8.59 -5.30 5.36	-11.4 -8.91 9.01
TF5A - T 34		-.400 -2.94 3.31	.310 -.231 -.311	1.36 1.85 1.78	1.16 1.04 1.05	-1.04 1.95 2.13	-3.86 -3.74 3.31	-8.70 -4.75 4.79	-10.9 -8.41 6.63
HT1A - TC 1		-2.81 -8.08 6.24	.120 -.678 1.18	1.12 .283 .800	11.6 6.87 6.82	7.88 12.0 12.3	-4.61 -2.48 3.86	-6.71 -8.82 6.88	-11.1 -9.04 9.13
HT2A - TC 3		-2.43 -4.81 4.70	1.84 -.143 1.36	4.43 3.95 4.03	6.79 4.73 4.77	-1.23 3.41 4.16	-3.78 -1.43 2.84	-5.20 -4.48 4.61	-10.6 -8.04 8.17
HT3A - TC 5		-6.37 -6.43 6.60	-3.20 -3.93 3.97	-.300E-01 -1.65 1.90	-1.05 -.338 .811	-3.79 -1.68 1.64	-8.11 -4.23 4.30	-7.34 -8.99 6.03	-12.1 -9.61 9.70
HT4A - TC 9		-2.81 -3.07 3.13	-1.66 -2.14 2.10	-.180 -1.13 1.24	-.360 -.269E-01 .202	-2.70 -.913 1.22	-3.72 -3.61 3.62	-6.05 -4.68 4.73	-10.4 -8.15 6.26
HT5A - TC12		-1.80 -1.54 1.67	-1.26 -1.86 1.67	-.710 -.852 .816	-.430 -.607 .647	-2.09 -.897 .891	-3.50 -3.22 3.28	-5.58 -4.41 4.47	-10.6 -8.06 8.18
HT6A - TC15		-1.43 -1.21 1.25	-1.31 -1.28 1.29	-1.28 -1.26 1.27	-.680 -.920 .851	-1.80 -.868 .816	-3.42 -3.07 3.12	-5.65 -4.40 4.46	-.830 -7.14 7.35
ML1A - X671		-.348 -.334 335.	-.347 -.347 348.	-.342 -.344 344.	-.336 -.339 339.	-.328 -.331 331.	-.330 -.330 330.	-.327 -.328 328.	-.326 -.326 326.
HP1A - X801		-.278E-01 -.273E-02 .351E-01	.813E-02 .230E-02 .899E-02	-.851E-02 .602E-03 .468E-02	.324E-02 -.276E-03 .322E-02	-.730E-03 .104E-02 -.180E-02	-.188E-02 -.182E-02 -.193E-02	-.807E-02 -.173E-02 -.384E-02	-.960E-02 -.756E-02 -.764E-02

Case B

CALCULATION-TO-EXPERIMENT DATA UNCERTAINTY ANALYSIS FOR NRC/ICAP.

FIRST LINE : DIFFERENCE BETWEEN CALCULATED AND (AVERAGED) EXPERIMENTAL DATA AT END OF THE INTERVAL
SECOND LINE : MEAN DIFFERENCE OVER THE INTERVAL
THIRD LINE : MEAN SIGMA OVER THE INTERVAL (ROOT MEAN SQUARE OF THE DIFFERENCE)

Table with columns for CODES, TIME INTERVAL, and various time points (e.g., 12.00, 30.00, 48.00, 66.00, 84.00, 102.00). Rows list various codes like P 18 - P 3, P 20 - P 4, etc., with numerical values for each time point.

1986-09-17

Case C

CALCULATION-TO-EXPERIMENT DATA UNCERTAINTY ANALYSIS FOR BRC/ICAP.

FIRST LINE : DIFFERENCE BETWEEN CALCULATED AND (AVERAGED) EXPERIMENTAL DATA AT END OF THE INTERVAL
 SECOND LINE : MEAN DIFFERENCE OVER THE INTERVAL
 THIRD LINE : MEAN SIGMA OVER THE INTERVAL (ROOT MEAN SQUARE OF THE DIFFERENCE)

- CODES -		- - - - TIME INTERVAL - - - -							
CALC.	EXP.	0.0 - 6.00	12.00	20.00	30.00	45.00	60.00	135.0	
P 1C - P 3		.170E-01 -.228E-01 .416E-01	.087E-01 .061E-01 .170E-01	.096E-01 .020E-01 .046E-01	.132 .110 .130	.066E-01 .133 .135	-.109 -.760E-01 .058E-01	-.221 -.168 .169	-.314 -.289 .304
P 2C - P 4		.074E-01 .142E-01 .368E-01	.107 .081E-01 .064E-01	.108 .121 .122	.107 .101 .162	.000E-01 .170 .172	-.006E-01 -.072E-01 .760E-01	-.197 -.121 .135	-.288 -.251 .253
P 3C - P 6		1.05 1.29 1.40	.040E-01 .120 .224	.123 .110 .111	.184 .137 .137	.780E-01 .185 .150	-.074E-01 -.023E-01 .740E-01	-.107 -.139 .143	-.300 -.263 .265
PD4C - D 4		1.88 4.36 0.62	1.22 1.34 1.36	1.08 1.03 1.06	1.07 1.08 1.05	2.20 1.70 1.00	1.00 3.24 3.47	.215 .600 .008	.134 .263 .207
PDLC - D LP		.371 .287 .284	.340 .335 .335	.353 .283 .263	.251 .282 .252	.014 .308 .400	-.310 -.040E-01 .108	.109 -.240 .355	.104 .150 .270
PDCC - D CO		-1.91 -1.68 1.03	-1.74 -2.04 2.05	-1.13 -1.27 1.39	-2.11 -1.00 1.81	-6.78 -3.27 2.69	-.000E-02 -4.58 4.00	-3.88 -2.41 2.04	-0.93 -0.50 0.06
PDUC - D LP		-.253 -.406 .052	-.265 -.349 .258	-.242E-01 -.204 .240	-.094E-01 -.052E-01 .055	-.303 -.492 .275	-.289 -.073 .603	-.633 -.378 .414	-.650 -.264 .460
PDDC - D DF		-.200E-01 -.909 1.79	-.118 .103E-01 .158	2.21 1.09 1.31	3.52 2.04 2.86	6.43 8.39 6.56	1.97 2.40 4.18	10.4 0.68 9.25	12.9 11.8 11.8
PDSC - D S6		-.494 .010 1.76	-1.49 -1.16 1.19	-1.73 -1.93 1.93	-2.11 -1.01 1.92	-.921 -1.08 2.08	-.380 -.448 .729	-.010 -.006 .034	-.033 -.929 .933
DF1C - X602		-.073E-01 .120E-01 .735E-01	-.067E-01 -.087E-01 .064E-01	.109 .218E-01 .020E-01	.610E-01 .700E-01 .700E-01	-.108 .136E-01 .611E-01	-.132 -.131 .293	-.241 -.139 .143	-.179 -.102 .188
DF2C - X603		-.193 -.186 .226	-.218E-01 -.121 .130	-.003 -.131 .108	-.250E-01 -.140 .100	-.290 -.106 .201	-.130 .207E-01 .082	-.284 -.309 .694	1.09 .309 .694
DF3C - X604		-.232 -.190 .213	-.261 -.247 .247	-.207 -.293 .293	-.242 -.272 .273	-.434 -.293 .298	.407 .630 .746	.017E-01 .129 .212	-.195 -.229 .267
DF5C - X607		.966E-01 .118 .184	.101 .104 .104	.020E-01 .086E-01 .087E-01	.023E-01 .040E-01 .049E-01	.410E-01 .091E-01 .101	-.110E-02 -.111E-01 .160E-01	-.771E-02 -.204E-02 .006E-02	-.163E-01 -.110E-01 -.173E-01
DF4C - X610		.151 .648 .640	-.091E-01 -.741E-01 .050E-01	-.133 -.090E-01 .104	-.282 -.108 .200	1.16 .141 .062	.817 .608 1.06	1.00 .634 .787	-.048 -.834 .042
DF6C - X636		-.606 -6.48 7.40	.800E-01 -.278 .323	.002E-01 .124E-01 .064E-01	.200 .165 .170	-.632 .242 .379	-.007E-01 -.222E-01 .140	.020E-01 .130 .708E-01	-.558E-01 .106E-01 .708E-01
TF1C - T 3		2.11 1.84 1.64	1.06 1.91 1.64	2.20 2.34 2.38	1.17 2.07 2.15	2.71 2.29 2.43	1.48 2.07 2.14	-.270 .741 .071	-4.25 -2.61 2.69
TF2C - T 14		1.63 1.82 1.87	2.76 2.06 2.11	1.38 1.87 1.60	3.42 2.89 2.69	2.70 3.47 3.93	.270 .024 1.12	-3.00 -.711 1.09	-6.70 -3.89 4.18
TF4C - T 16		2.87 1.84 1.71	3.79 3.60 3.52	2.23 2.74 2.82	2.07 2.75 2.76	1.00 3.06 3.12	-.230 .445 .012	-2.89 -1.05 1.42	-6.75 -4.28 4.43
TF3C - T 31		-6.76 .365 .675	6.70 3.79 4.45	6.00 6.28 6.37	0.88 6.05 6.22	3.20 0.70 9.96	-2.48 -1.43 2.05	-3.46 -3.32 3.39	-4.06 -6.28 9.37
TF5C - T 34		-2.26 -6.45 6.12	-1.09 -1.71 1.74	-.630 -.023E-01 .083	-.190 -.108 .707	1.01 1.61 1.75	-1.02 -1.09 1.79	-3.67 -2.77 2.02	-7.62 -8.81 6.93
HT1C - TC 1		-2.70 -6.12 6.28	-1.17 -1.42 1.02	-1.20 -1.89 1.70	6.81 3.09 4.02	9.87 10.0 10.1	-3.06 -1.09 1.25	-4.73 -3.77 3.01	-7.93 -6.04 0.61
HT2C - TC 3		-2.36 -4.90 4.71	2.06 -.840E-01 1.38	4.48 3.74 3.60	6.87 6.88 6.81	.790 4.97 6.38	-1.70 -1.81E-01 2.11	-3.25 -2.60 2.68	-7.44 -8.54 6.66
HT3C - TC 6		-6.25 -6.45 6.84	-2.08 -3.78 3.64	.190 -1.62 1.79	.600E-01 .665 .954	-1.74 -.747E-01 .661	-3.85 -2.78 2.09	-6.38 -4.14 4.19	-6.91 -7.11 7.20
HT4C - TC 9		-2.78 -3.19 3.24	-1.35 -1.95 2.01	.200 -.826 .976	.780 .073 .600	-.740 .703 .930	-2.21 -2.18 2.20	-4.08 -2.83 2.69	-7.18 -6.68 6.77
HT5C - TC 12		-1.80 -1.69 1.79	-.090 -1.38 1.42	-.230 -.472 .697	.730 .261 .426	-.180 1.00 1.13	-2.01 -1.76 1.09	-3.61 -2.87 2.64	-7.60 -6.59 6.70
HT6C - TC 15		-1.28 -1.18 1.22	-.040 -1.00 1.02	-.700 -.741 .764	.070 -.616E-01 .604	-.600E-01 .046 .635	-1.06 -1.57 1.70	-3.83 -2.53 2.60	-7.12 -6.40 6.80
DL1C - X671		-.351 -.336 .336	-.383 -.352 .362	-.353 -.353 .353	-.351 -.352 .352	-.347 -.349 .349	-.348 -.349 .349	-.344 -.346 .346	-.344 -.343 .343
HP1C - X601		-.278E-01 -.848E-02 .396E-01	.010E-02 -.288E-02 .808E-02	-.851E-02 -.602E-02 .466E-02	-.324E-02 -.178E-02 .322E-02	-.730E-02 -.104E-02 .190E-02	-.180E-02 -.167E-02 .193E-02	-.607E-02 -.378E-02 .264E-02	-.854E-02 -.756E-02 .754E-02

1986-09-17

Description for the accompanying data package

STUDSVIK

THIS TAPE CONTAINS DATA FROM THE ICAP PREDICTION CALCULATION
WITH THE RELAP5/MOD2/36.04 FOR THE FIX-II EXPERIMENT NO. 3051.

CONTENTS. FILE	1.	THIS DESCRIPTIVE TEXT
	2.	INPUT CASE A, STEADY STATE
	3.	" - " B, " - "
	4.	" - " C, STEADY STATE
	5.	DATA, EXPERIMENT
	6.	" - " , CASE A
	7.	" - " , CASE B
	8.	" - " , CASE C

I. COMPUTER

NAME	CYBER 170-810
WORD SIZE	60

II. TAPE FORMAT

NUMBER OF TRACKS	9
PACKING DENSITY	1600 BPI
RECORD SIZE	80
BLOCKING FACTOR	64
CODED	EBCDIC
CONTROL WORDS	NO

III. DATA FORMAT. FOR EACH OF THE FILES 5 THROUGH 8

TITLE RECORD(S). (FORMAT I5,A75)

FIELD 1. THE NUMBER OF DATA CHANNELS ON THE FILE

FIELD 2. PROBLEM IDENTIFICATION

UP TO FIVE ADDITIONAL IDENTIFICATION RECORDS

MAY BE ADDED BY 'C' IN COLUMN 1 OF FIELD 2

DATA SET RECORD 1. (FORMAT 2I5,A60)

FIELD 1. NUMBER OF DATA POINTS

FIELD 2. THE ENGINEERING UNIT CODE (EUC) FOR THE
VARIABLE

FIELD 3. IDENTIFYING TEXT OF THE DATA

REMAINING DATA SET RECORDS FORMAT 5(E16.9)

EACH DATA CHANNEL SUBMITTED IS GIVEN THROUGH TWO DATA
SETS. THE FIRST OF WHICH IS THE TIME DATA SET.

THE TWO SETS HAVE THE SAME NUMBER OF DATA POINTS.

THE TIME DATA SET IS IDENTIFIED BY EUC-77 (FIELD 2)

AND THE IDENTIFYING TEXT 'TIME' (FIELD 3).

BIBLIOGRAPHIC DATA SHEET

(See instructions on the reverse)

1. REPORT NUMBER
(Assigned by NRC. Add Vol., Supp., Rev.,
and Addendum Numbers, if any.)

NUREG/IA-0029
STUDSVIK/NP-86/108

2. TITLE AND SUBTITLE

Assessment of RELAP5/MOD2, Cycle 36.04 Against FIX-II
Split Break Experiment No. 3051

3. DATE REPORT PUBLISHED

MONTH	YEAR
October	1989

4. FIN OR GRANT NUMBER

5. AUTHOR(S)

John Eriksson

6. TYPE OF REPORT

7. PERIOD COVERED (Inclusive Dates)

8. PERFORMING ORGANIZATION - NAME AND ADDRESS (If NRC, provide Division, Office or Region, U.S. Nuclear Regulatory Commission, and mailing address. If contractor, provide name and mailing address.)

Swedish Nuclear Power Inspectorate
S-61182 Nykoping, Sweden

9. SPONSORING ORGANIZATION - NAME AND ADDRESS (If NRC, type "Same as above"; if contractor, provide NRC Division, Office or Region, U.S. Nuclear Regulatory Commission, and mailing address.)

Office of Nuclear Regulatory Research
U. S. Nuclear Regulatory Commission
Washington, DC 20555

10. SUPPLEMENTARY NOTES

11. ABSTRACT (200 words or less)

The FIX-II split break experiment No. 3051 has been analyzed using the RELAP5/MOD2 code. The code version used, Cycle 36.04, is the frozen version of the code.

Three calculations were carried out to study the sensitivity of various parameters to the change of break discharge and passive heat structures. The differences between the calculations and the experiment have been quantified over intervals in real time for a number of variables available from the measurements during the experiment.

12. KEY WORDS/DESCRIPTORS (List words or phrases that will assist researchers in locating the report.)

RELAP, ICAP Program, Split Break

13. AVAILABILITY STATEMENT

Unlimited

14. SECURITY CLASSIFICATION

(This Page)

Unclassified

(This Report)

Unclassified

15. NUMBER OF PAGES

16. PRICE

UNITED STATES
NUCLEAR REGULATORY COMMISSION
WASHINGTON, D.C. 20555

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ASSESSMENT OF RELAP5/MOD2, CYCLE 36.04 AGAINST FIX-II SPLIT
BREAK EXPERIMENT NO. 3051

OCTOBER 1989