

CALCULATION DATA/TRANSMITTAL SHEET

DOCUMENT IDENTIFIER

CALC. 32 - 9745 - 00

TRANS. 86 - _____ - _____

TYPE: RESEARCH & DEVELOPMENT SAFETY ANALYSIS REPORT NUC. SERV. INPUT DESIGN REQ'T. DESIGN VERIF. OTHER

TITLE Pressurizer Level Change Due to MakeUp Flowrate

PREPARED BY R.W. Winks

REVIEWED BY R.M. H...-m...

TITLE Principal Engineer

DATE 10/2/78

TITLE Senior Engineer

DATE 10/2/78

PURPOSE:

To amend an existing calc file and report submitted to TECO predicting Pressurizer level changes after reactor trips at Davis-Besse 1. This report is to account for a net makeup flowrate into the RC System and its effect on the change in Pressurizer level.

SUMMARY OF RESULTS (INCLUDE DOC. ID'S OF PREVIOUS TRANSMITTALS & SOURCE CALCULATIONAL PACKAGES FOR THIS TRANSMITTAL)

References:

Calculational File: 32-9538-00 by R.W. Winks
 Transmittal Document: 86-2226-00 by R.W. Winks

Summary:

Corrections to Calculated Per level Change (Table 2 of 86-2226-00) are shown below:

Rx Trip Date	Calculated Per level	Correction to Calc. Per Level
2/24/78	184	8.3
4/2/78	167	8.2
8/2/78	206	22.9
11/29/77	181	14.7

DISTRIBUTION:

POOR ORIGINAL

BABCOCK & WILCOX
GENERAL CALCULATIONS

Problem: The results of calculating Pressurizer level change during reactor trip transients at Davis-Besse 1 did not contain any account of net makeup flowrate into the RC system which will in turn affect the final pressurizer level.

Review all available RC System flowrate data during the four reactor trips analyzed in my Calculational File 32-9538-00 and transform the net volume added during the transient into equivalent pressurizer level change.

The simple pressurizer level-RC volume model used in Calculational File 32-9538-00 assumed mass in the RC system as constant.

This study shall determine the correction that could be applied to the calculated change in pressurizer level during a reactor trip transient due to the net addition of makeup flow into the RC System.

Approach:

After achieving agreement with TECO Engineering on validity of measured flowrates, use Post-Trip Review log data to determine profile of net makeup flowrate according to the expression:

$$W_{net} = W_{cool\ injection} + W_{makeup} - W_{loss}$$

and integrate this over period to reach minimum pressurizer level to obtain volume added to RCS. Then, account for density change as 100°F water is heated to equilibrium with cold leg temperature in the RCS. Add a final column to Table "2" in my Transmittal package 86-2226-00.

CUSTOMER TECO

PROP NO

FILE NO

SUBJECT Per Level Due to MakeUp Flow

DWG NO

COMP NO

CONT NO 520.00 14

GROUP NO

CALC BY R. W. Winks

DATE 10/3/78

SHEET NO 2 of 22

BABCOCK & WILCOX
GENERAL CALCULATIONS

Post Trip Review Log

Reactor Trip Time from Alarm Printer (SIR-431 File)
= 05:51:06

Clock Time	Net Time	F-740 H.U. Flow gpm	F-717 Letdown Flow gpm	F-782 Seal Inject Flow-gpm	RC Pressure psig	
05:50:00	-66	-	54.45	-		
05:50:15	-51	16.53	"	36.38	2153	
05:50:30	-36	"	54.36	"	"	
05:50:45	-21	29.24	"	35.71	2146	
05:51:00	-6	"	54.19	"	"	
(05:51:06)	0	-	-	-	2155	
05:51:15	9	38.60	"	34.92	2140	
05:51:30	24	"	54.05	"	"	
05:51:45	39	(- \$)	"	22.35	1750 1770	330
05:52:00	54	(- \$)	46.62	"	1720 "	330
05:52:15	69	(- \$)	"	24.25	1725 1743	330
05:52:30	84	(- \$)	0.0	"	"	330

Note: At 31 seconds (net) the second makeup pump was turned on.

(- \$) symbol means off-scale (maximum flowrate)

On Telephone call on Sept 26, 1978 Sushil Jain (TECO) stated that maximum flowrate for 3 H.U pumps will be 330 gpm at 1800 psig or 290 gpm at 1900 psig RC Pressure.

(Assume 340 gpm at 1700 psig) Appendix FIG 6

Assume H.U. Flow temperature is approximately 100 F as is letdown flowrate and seal injection flowrate. Therefore, net flowrate will be measured at approximately 100 F but will expand to a larger flowrate after injected into the RCS.

POWER TECO	PROP NO	FILE NO
SUBJECT PZR LEVEL DUE TO MakeUp Flow	DWG NO	COMP NO
CONT NO 620.00/14	GROUP NO	
CALC BY R. W. Winks	DATE 9/28/78	SHEET NO 3 of 22
CHECK BY	DATE	

POOR ORIGINAL

BABCOCK & WILCOX
GENERAL CALCULATIONS

Reactor Trip on 2/24/78 (SPR # 431)

$$\dot{W}_{net} = \dot{W}_{SI} + \dot{W}_{MU} - \dot{W}_{LD}$$

Time sec	\dot{W}_{SI} gpm	\dot{W}_{MU} gpm	\dot{W}_{LD} gpm	\dot{W}_{net} gpm
0	35	36	54	17
31	25	45	52	18
35	23	330	51	302
60	23	330	37	316

Volume of net makeup flow into RCS at 100°F:

$$Vol = \frac{31}{60} (17.5) + \frac{4}{60} (18 + 142) + \frac{25}{60} (309) \text{ gallons}$$

$$= 9.0 + 10.7 + 128.75 = 148.5 \text{ gallons}$$

At time of minimum pressurizer level ($t + 60$ seconds)

RC pressure = 1740 psia (Reactimeter)

and $T_{cold} = 550 F$

$$\rho_{cold} \text{ m.v.} = 62.32 \text{ lbs/ft}^3 @ 100 F$$

$$\rho_{hot} \text{ r.c.} = 46.50 \text{ lbs/ft}^3 @ 550 F$$

$$\text{Density ratio} = 1.34$$

Volume of 550 F water added into RC System is:
 $1.34 \times 148.5 = 199 \text{ gallons}$

$$\Delta \text{ PZR level} = \frac{199}{7.4805 \times 3.2} = 8.3 \text{ inches}$$

OWNER TECO

PROP NO

FILE NO

SUBJECT PZR LEVEL DUE TO MAKEUP FLOW

DWG NO

COMP NO

CONT NO 620-0014

GROUP NO

CALC BY R. W. Winks

DATE 9/28/78

SHEET NO 4 of 22

CHECK BY

DATE

POOR ORIGINAL

RC SYSTEM FLOWRATES AFTER REACTOR TRIP ON
FEB 24, 1978 AT DAVIS-BESSE 1

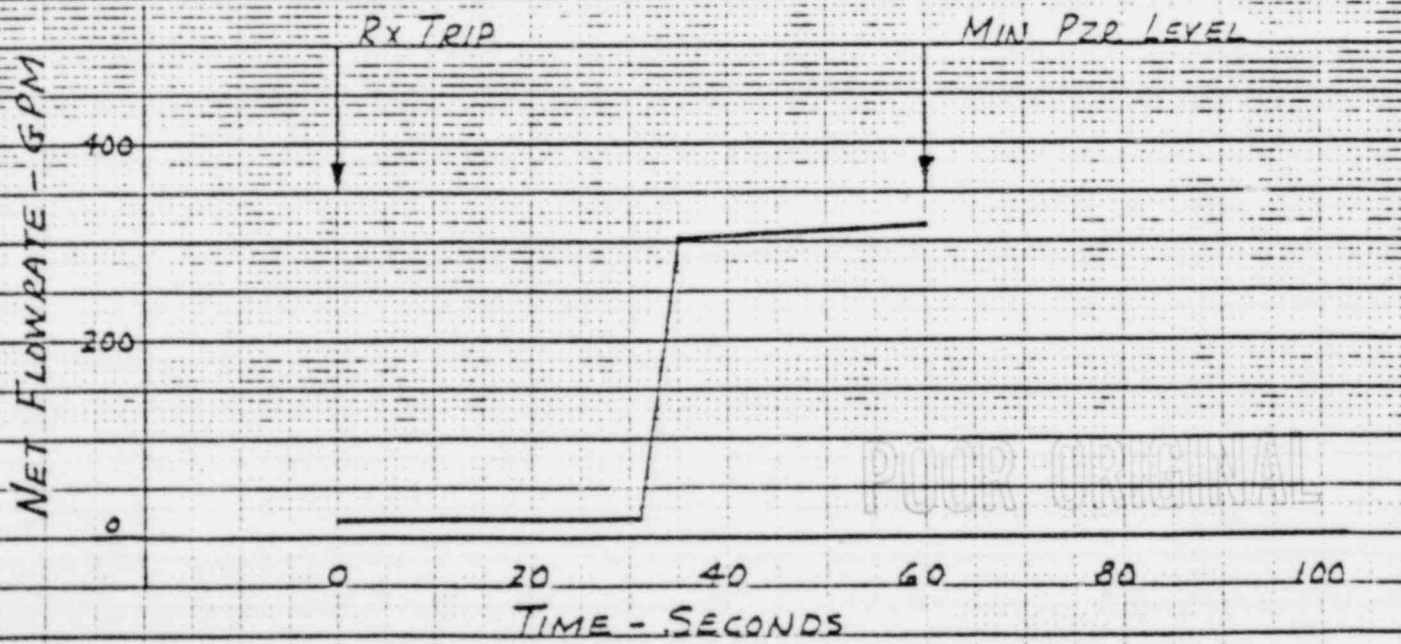
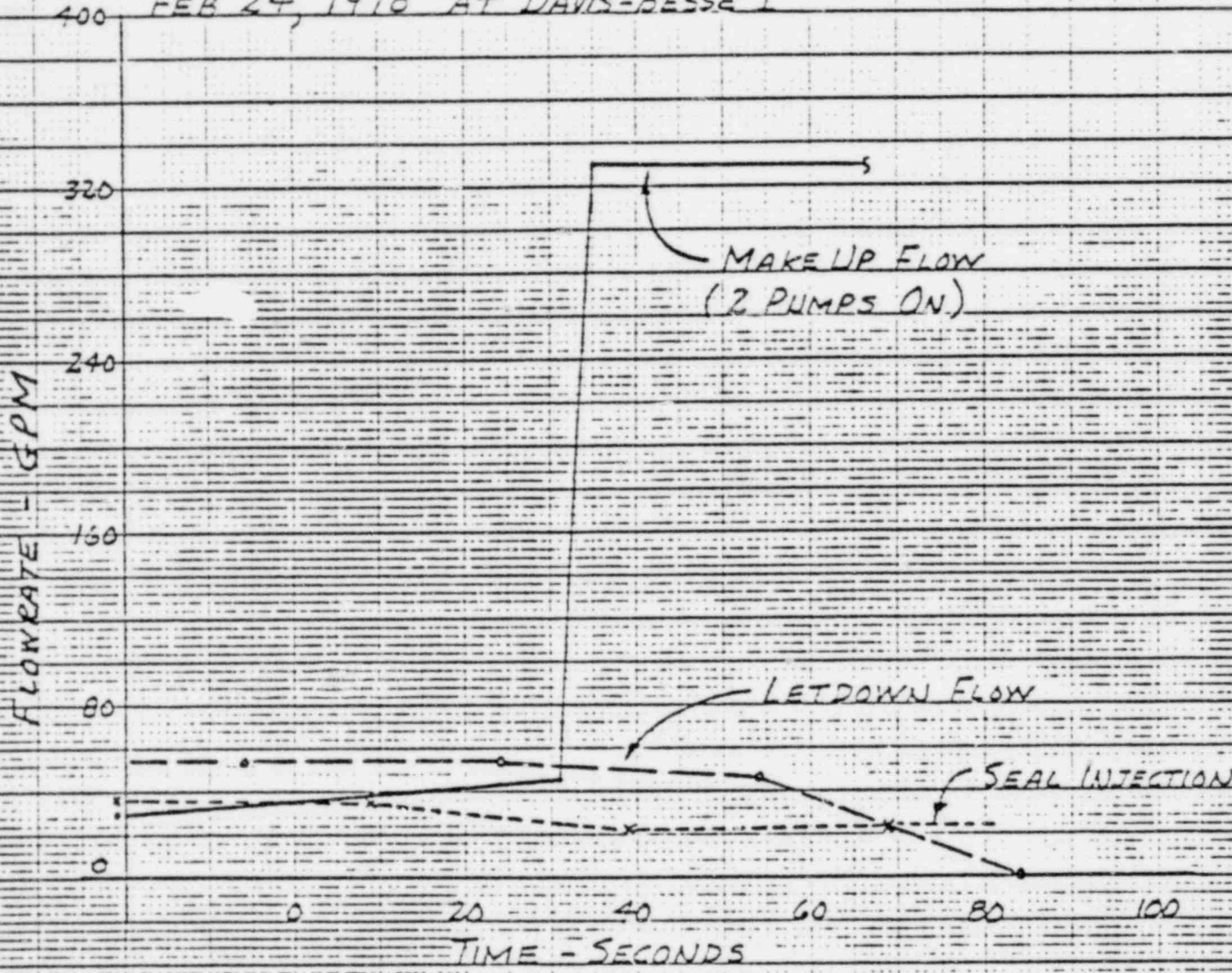


FIG 1

46 1470

K-E 10 X 10 10 1/2 INCHES
REINFORCED & ESSENCE
MADE IN U.S.A.

BABCOCK & WILCOX
GENERAL CALCULATIONS

Post Trip Review log for 4/2/78 Rx Trip
SPR # 435

Rx Trip Time = 8:30:12 (Phone call from S. Jain)

Clock Time	Net Time	F-740 H.U. Flow	F-717 l.d. Flow	F-782 Seal Inj Flow	RC Press	Calc H.U. Flow
08:29:30	-42	27.8	-	-	2189	
08:29:45	-27	"	57.6	33.36	"	
08:30:00	-12	16.7	"	36.68	2048	
08:30:12	0	"	"	"	"	
08:30:15	3	"	136.5	"	"	
08:30:30	18	-5	"	"	1710	(225) *
08:30:45	33		52.9	21.6	"	(346)
08:31:00	48		"	"	1653	(350)
08:31:15	63		0	33.07	"	(350)

TECO said #2 MU Pump started 22 seconds after Rx Trip

* To be conservative let us assume at 18 seconds 1 mu pump is on but valve is wide open and flow is 225 gpm. Then, at 22 seconds mu pump #2 is started and by 25 seconds flow is 340 gpm.

$W_{net} = W_{st} + W_{mu} - W_{ld}$

Time	W _{st}	W _{mu}	W _{ld}	W _{net}
Sec	gpm	gpm	gpm	gpm
0	33	13	57	-11
3	32	50	136	-54
18	28	225	93	+160
25	26	340	74	292
45	26	348	31	343
10	30	132	116	+46

POOR ORIGINAL

C OVER TECO
SUBJECT: P&R LEVEL DUE TO MAKE UP FLOW
CONT NO 520 00:14
CALC BY R.W. Winks

PROP NO:
DWG NO:
GROUP NO:
FILE NO:
COMP NO:
SHEET NO 6 of 22

DATE 10/2/78

BABCOCK & WILCOX
GENERAL CALCULATIONS

4/2/78 Ex Trip Continued

Volume of net makeup flow added to RCS:

$$Vol = \frac{-3}{60} \left(\frac{54}{2} \right) - \frac{4}{60} \left(\frac{54}{2} \right) + \frac{18}{60} \left(\frac{292}{2} \right) + \frac{20}{60} \left(\frac{292+343}{2} \right)$$

$$= -3 + 44 + 106 = 147 \text{ gallons (at 100 F)}$$

At time of minimum pressurizer level RC pressure was 1665 psia and Temp was 550 °F

$$\rho_{\text{cold at 100 F}} = 62.32 \text{ lbs/ft}^3$$

$$\rho_{\text{hot at 550 F \& 1665 psia}} = 46.45 \text{ lbs/ft}^3$$

$$\text{Density ratio} = 1.34$$

Volume of water added to RCS at 550 F is:

$$1.34 \times 147 = 197 \text{ gallons}$$

$$\Delta \text{ PZR level} = \frac{197}{7.4805 \times 3.2} = 8.2 \text{ inches}$$

POOR ORIGINAL

CUSTOMER TECO

PROP NO

FILE NO

SUBJECT PZR LEVEL DUE TO MAKEUP FLOW

DWG NO

COMP NO

CONT NO 820-0014

GROUP NO

CALC BY R. W. Winks

DATE 10/2/78

SHEET NO 7 of 22

NET RC SYSTEM FLOW AFTER REACTOR TRIP ON
APRIL 2, 1978 AT DAVIS-BESSE 1

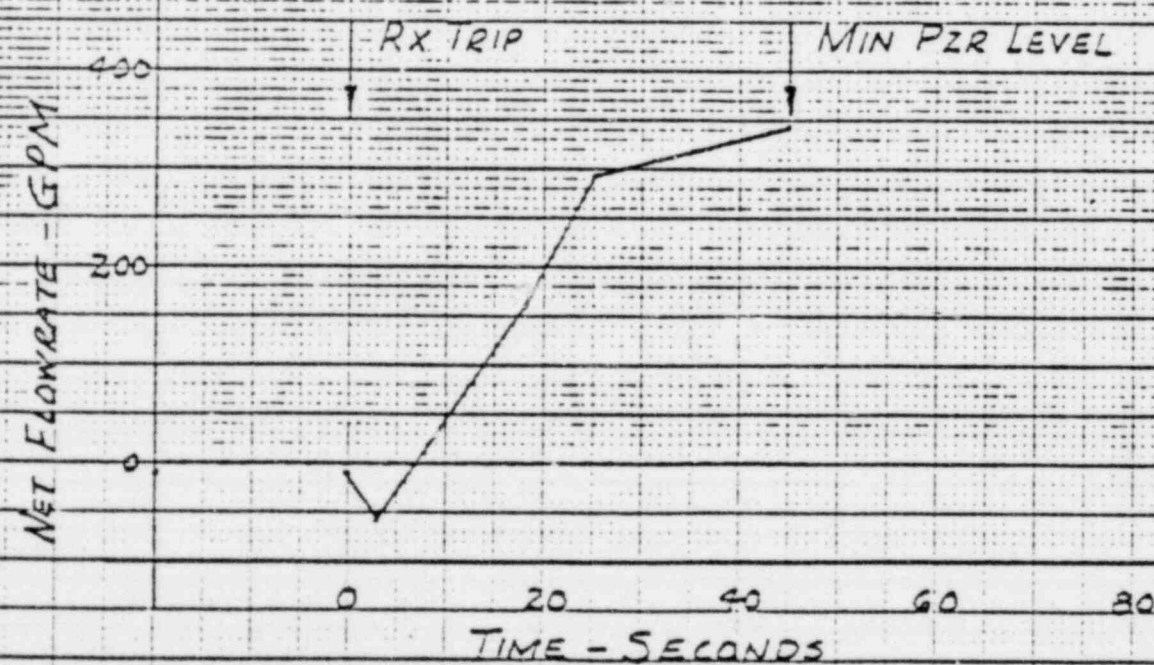
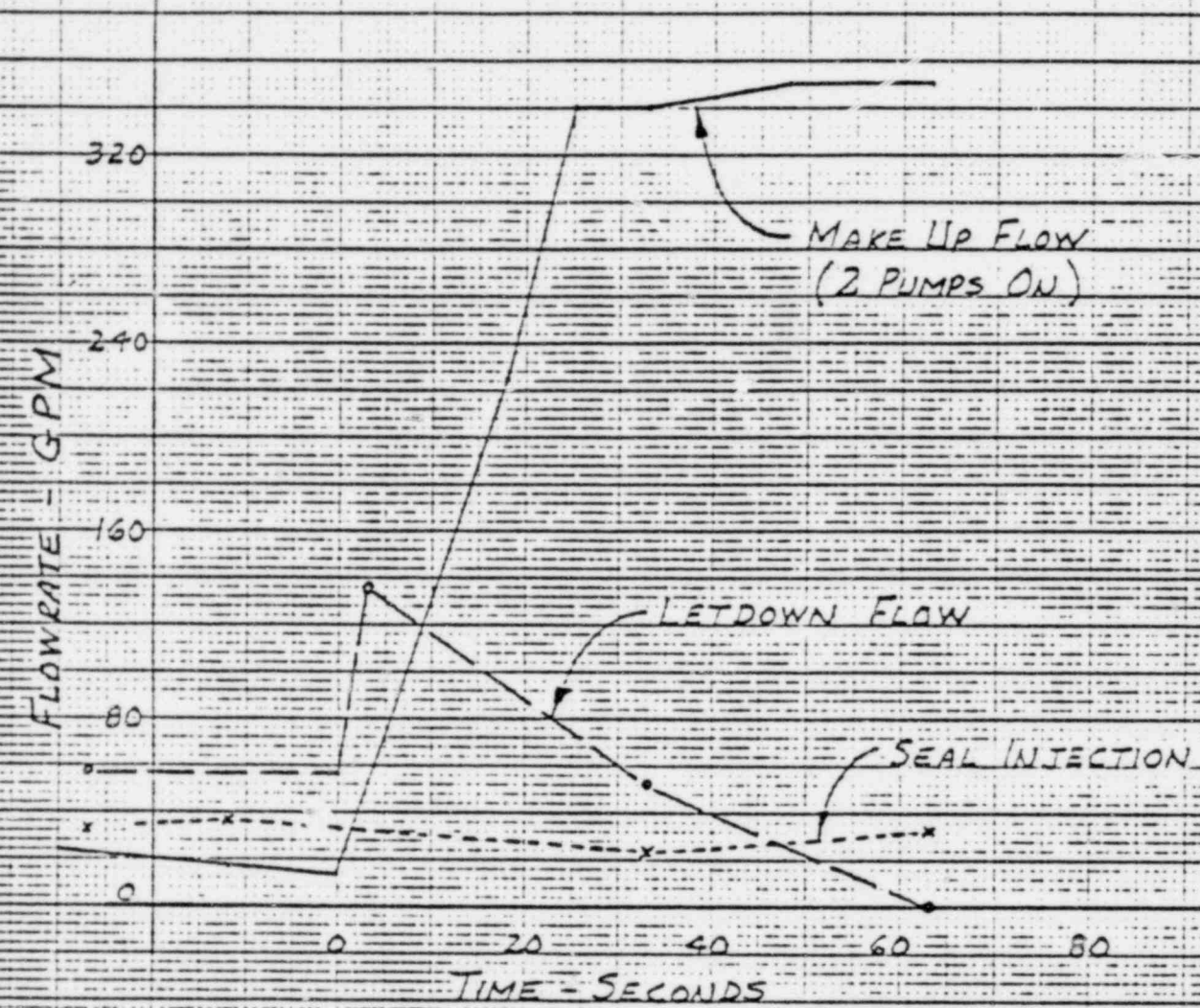


FIG 2

46 1470
K-E 10 X 10 TO 1/2 INCHES * 719 X 10 INCHES
NEUFEL & ESSER CO. MADE IN U.S.A.

**BABCOCK & WILCOX
 GENERAL CALCULATIONS**

Post Trip Review Log for Rx Trip on 8/2/78

Rx Trip Time 09:50:44 (Alarms Printer)
 * 2nd M.U. Pump m. 13 seconds after Rx Trip
 Past Trip Review Log Data:

Clock Time	Net Time	F-740 M.U. Flow	F-717 L.d. Flow	F-782 S.I. flow	RC Press	"Calc" M.U. Flow
		gpm	gpm	gpm	gpm	gpm
09:49:30	-74	19.3	90.7	38.4	2108	
09:49:45	-59	"	"	"	"	
09:50:00	-44	19.3	92.3	35.5	2238	
09:50:15	-29	"	"	"	"	
09:50:30	-14	13.5	92.3	37.2	2110	
09:50:45	+1	"	"	"	"	
* 09:51:00	16	(-3)	87.2	25.2	1869	(310)
09:51:15	31		"	"	"	"
09:51:30	46		38.9	35.3	1776	(327)
09:51:45	61		"	"	"	"
09:52:00	76		38.8	34.9	1783	(324)
09:52:15	91		"	"	"	"
09:52:30	106		39.1	34.2	1827	(318)
09:52:45	121	(-3)	"	"	"	"

$$W_{net} = W_{SI} - W_{mu} - W_{ld}$$

Time sec	W _{SI} gpm	W _{mu} gpm	W _{ld} gpm	W _{net} gpm
0	38	12	92	-42
16	25	310	97	+248
46	35	327	39	+323
90	35	322	39	+318

POOR ORIGINAL

C OVER <u>TECO</u> SUBJECT <u>PRR LEVEL DUE TO MAKE UP FLOW</u> CONT NO <u>020 00 14</u> CALC BY <u>R. W. Winks</u> CHKD BY _____	PROP NO _____ FILE NO _____ DWG NO _____ COMP NO _____ GROUP NO _____ DATE <u>10/2/78</u> SHEET NO <u>9 of 22</u> DATE _____
---	---

BABCOCK & WILCOX
GENERAL CALCULATIONS

Rx Trip of 8/2/78 Continued:

Volume added to EC System in 90 second period:

$$Vol = -\frac{2}{60} \left(\frac{42}{2} \right) + \frac{14}{60} \left(\frac{248}{2} \right) + \frac{30}{60} \left(\frac{248+323}{2} \right) + \frac{44}{60} \left(\frac{323+318}{2} \right)$$

$$Vol = -0.7 + 28.9 + 143 + 235 = 406 \text{ gallons}$$

Cold H.W. water density = 62.32 lbs/ft³ at 100F

Hot H.W. water density at 555F @ 1800 psia

(Page 25 of 55 in Calc File 32-9538-00 by RW Winks)

$$\rho_{hot} = 46.20 \text{ lbs/ft}^3$$

Density Ratio = 1.35

Volume of 555F net makeup volume = 548 gallons

Change in Per level due to net makeup volume:

$$\frac{548}{7.4805 \times 3.2} = 22.9 \text{ inches}$$

POOR ORIGINAL

OWNER <u>TECO</u>	PROP NO	FILE NO
SUBJECT <u>PER LEVEL DUE TO MAKEUP FLOW</u>	DWG NO	CUMP NO
CONT NO <u>520.00/4</u>	GROUP NO	
CALC BY <u>R. W. Winks</u>	DATE <u>10/2/78</u>	SHEET NO <u>10 of 22</u>
CHKD BY	DATE	

RC SYSTEM FLOWRATES AFTER REACTOR TRIP ON
AUG 2, 1978 AT DAVIS-BESSE I

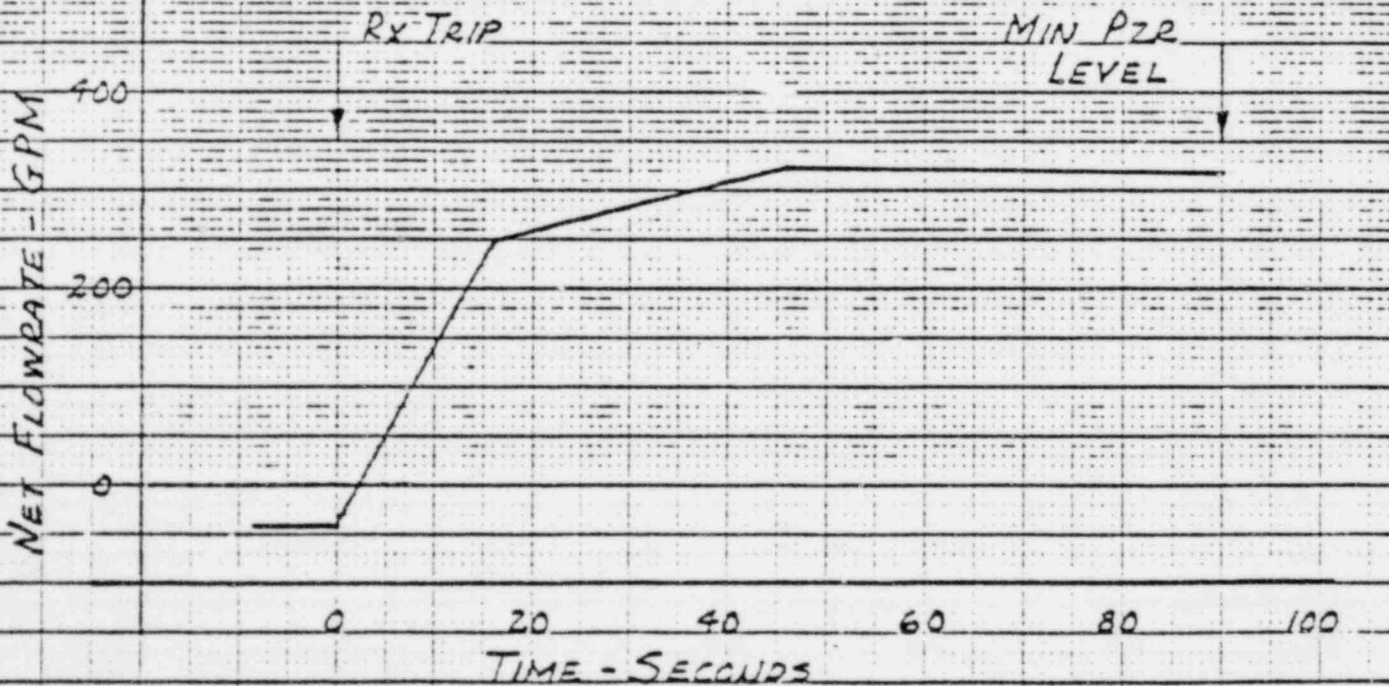
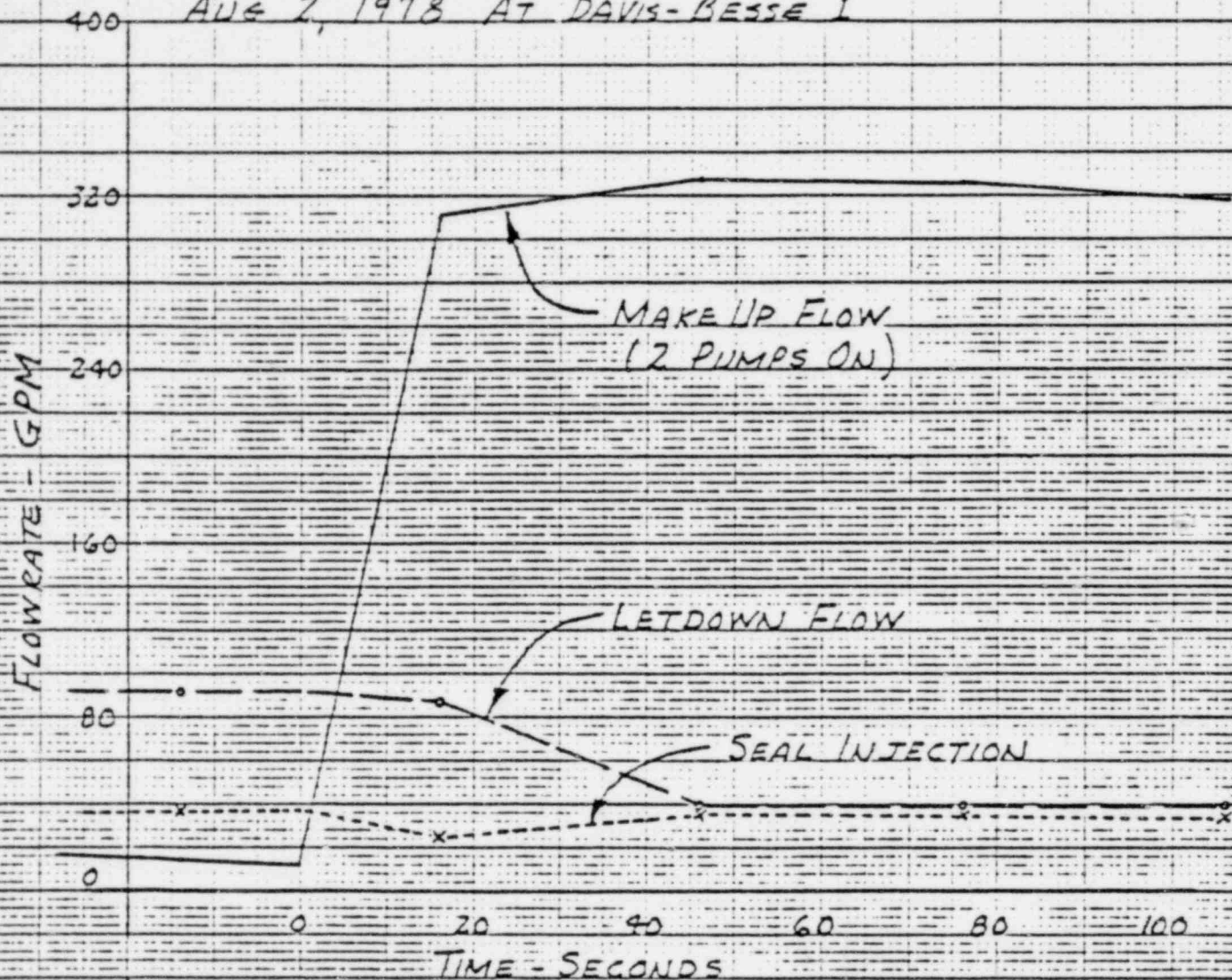


FIG 3

POOR ORIGINAL

46 1470

K-E 10 X 10 TO 15 INCH 3/4 X 10 INCHES
HEWLETT & PACKARD CO. MODEL 1000A

BABCOCK & WILCOX
GENERAL CALCULATIONS

Post Trip review for Ex Trip on Nov 29, 1977

Rx Trip Time 22:43:24 } See Alarm Printer Output
 #1 MU Pump on until 22:43:55 }
 #2 MU Pump started 22:46:52 (Single Pump Running)

Clock Time	Net Time	F-740	F-717	F-782	RC Press	Calc
	sec	MU Flow	l.d. Flow	S.I. Flow	psig *	H.U. Flow
22:42:30	-54	27.3	50.8	35.8		
22:43:00	-24	27.0	50.8	35.6		
22:43:24	0	—	—	—	2123	
22:43:30	6	125.6	50.8	24.8	2070	
22:43:45	21	"	50.7	"	1990	
22:44:00	36	119	"	(- \$)	1950	
22:44:15	51	"	0.0	"	"	
22:44:30	66 = (1.1)	16.1	0.0	"	1960	
22:45:30	126 = (2.1)	16.0	0.0	"	1935	
22:46:30	186 = (3.1)	15.8	0.0	(- \$)	1845	
22:46:52	208 = (3.47)	#2 Started				(220)
22:47:30	246 = (4.1)	18.0	0.0	"	1755	(220)
22:48:00	276 = (4.6)	"	"	26.4	1725	(225)
22:48:15	291 = (4.85)	18.0	0.0	"	1650	(233)
22:49:15	351 = (5.85)	18.0	0.0	27.2	1625	(235)

* Refer to Page 30/55 of Calc File 32-9538-00 by R.W. Winks

To be very conservative, assume one makeup pump is on at full flow at 22:46:52 time as shown in Alarm Printer but not indicated as M.U. Flow in Post Trip Review log.

POOR ORIGINAL

U. MES TECO	PROP NO	FILE NO
SUBJECT PZR LEVEL DUE TO MAKEUP FLOW	DWG NO	COMP NO
DNT NO 520.0014	GROUP NO	
ALC BY R. W. Winks	DATE 10/2/78	SHEET NO 12 of 22
HKO BY	DATE	

BABCOCK & WILCOX
GENERAL CALCULATIONS

Nov 29, 1977 Rx Trip

$W_{net} = W_{SI} + W_{mu} - W_{ld}$

Time min	W_{SI} gpm	W_{mu} gpm	W_{ld} gpm	W_{net}
0	28	27	51	+4
0.1	25	125	51	99
0.6	0	119	25	94
0.85	0	70	0	70
1.1	0	16	0	16
3.1	0	16	0	16
3.5	0	220	0	220
4.1	0	220	0	220
4.6	27	225	0	252
5.25	27	235	0	262

Volume Added to RC System between 0 & 4.0 Minutes:

$$Vol = 0.1 \left(\frac{100}{2} \right) + 0.5 (96.5) + 0.5 \left(16 + \frac{94-16}{2} \right) + 2.0 \times 16$$

$$+ 0.4 \left(16 + \frac{220-16}{2} \right) + 0.5 (220)$$

Note: At $T = 240$ seconds after Rx Trip $T_{cold} \approx 529 F$
(Ref.: Pg 30 of Calc File 32-9538-00 by RW Winks)

$Vol = 5.0 + 48.3 + 27.5 + 32 + 47.2 + 110$

$Vol = 270$ gallons

Density ratio = $\frac{62.32 \text{ lbs/ft}^3}{\rho_{HOT} @ 529 F \& 1640 \text{ psia}} = \frac{62.32}{47.78} = 1.304$

Volume Added to RCS at 529 F = $1.304 \times 270 = 352$ gallons

Δ Per level change = $\frac{352}{74805 \times 3.2} = 14.7$ Inches At 4.0 Minutes

POOR ORIGINAL

CUSTOMER <u>TECO</u>	PROP NO	FILE NO
SUBJECT <u>PER LEVEL DUE TO MAKEUP FLOW</u>	DWG NO	COMP NO
CONT NO <u>620.0014</u>	GROUP NO	
CALC BY <u>R. W. Winks</u>	DATE <u>10/3/78</u>	SHEET NO <u>13 of 22</u>

RC SYSTEM FLOWRATES AFTER REACTOR TRIP AND STATION BLACKOUT ON NOV 29, 1977

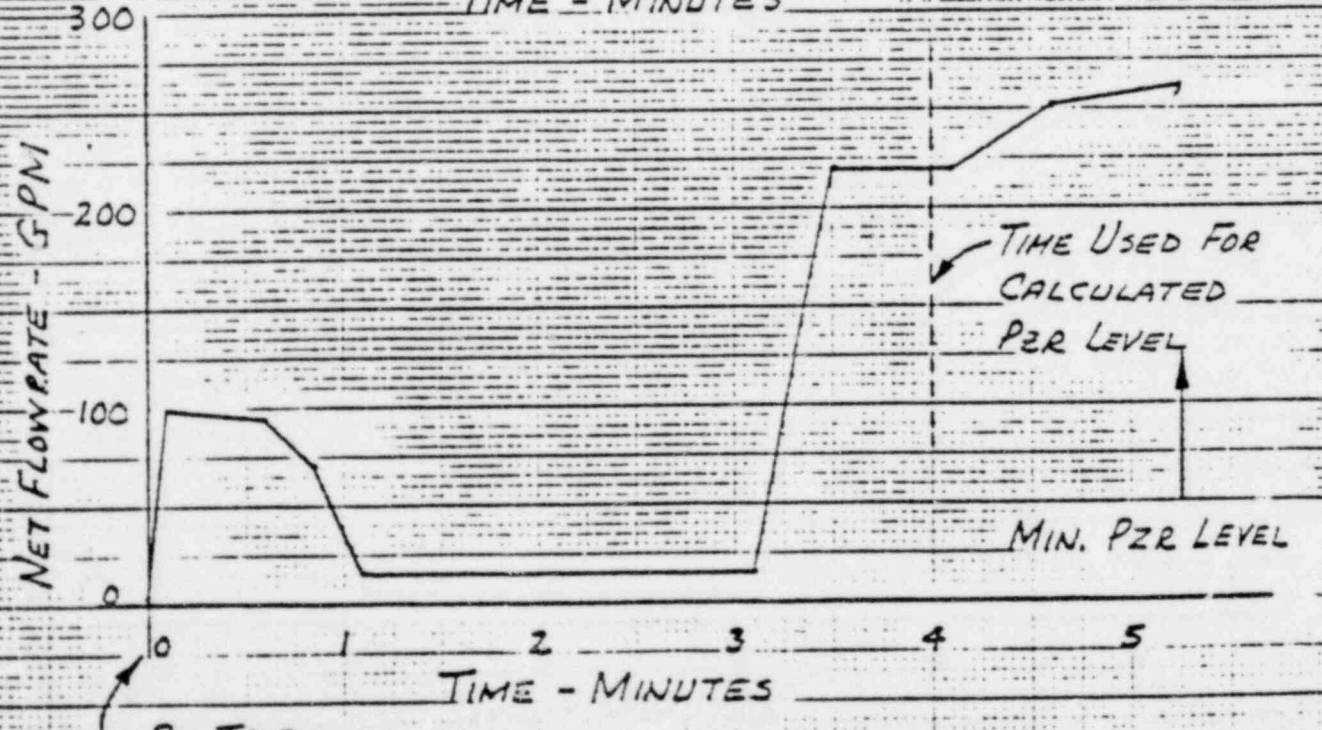
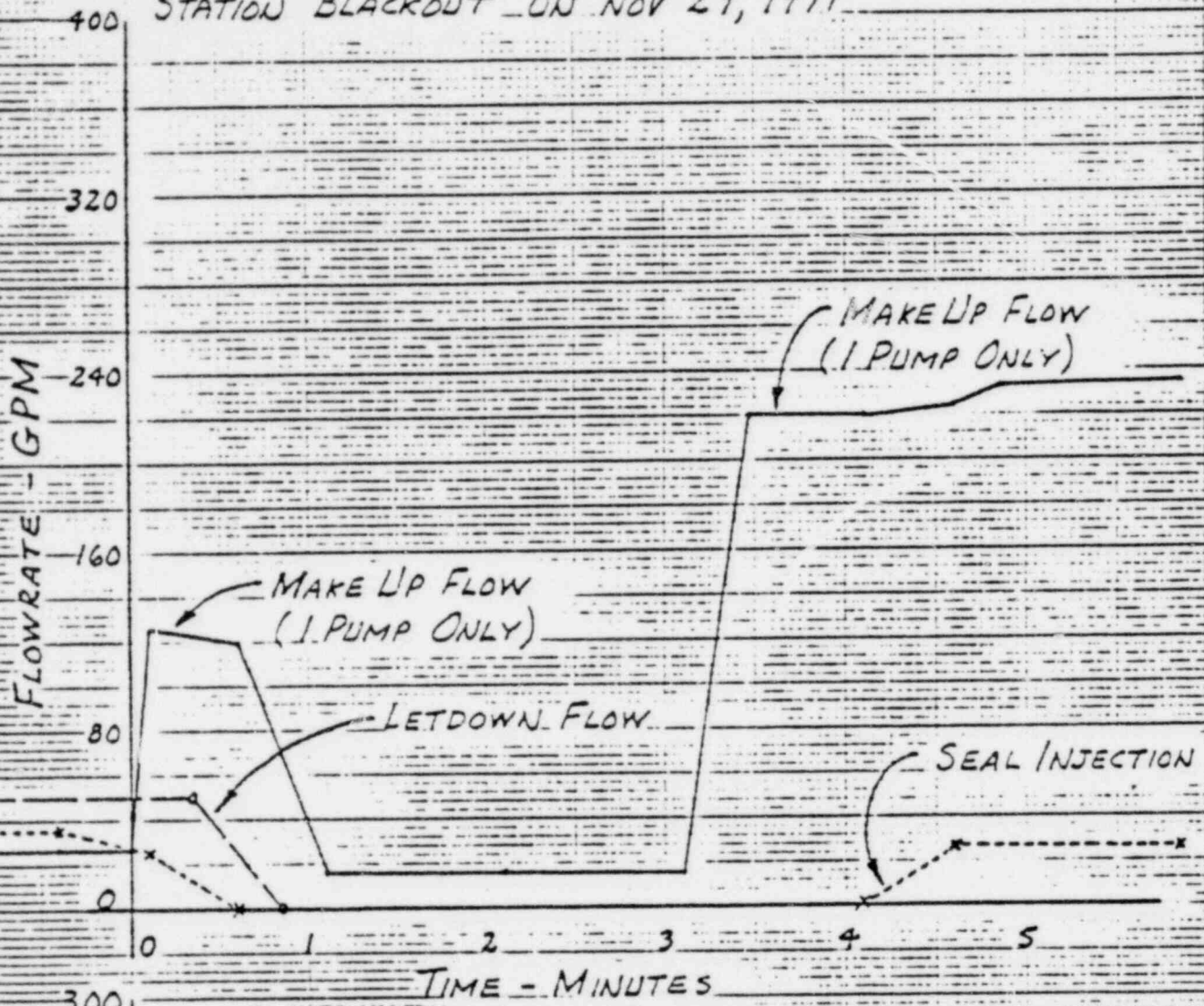


FIG 4

POOR ORIGINAL

46 1323

10 X 10 FO 3, 10X11 1, 1 X 10 10X11 5
NEUFEL & ESSER CO. MADE IN U.S.A.

**BABCOCK & WILCOX
 GENERAL CALCULATIONS**

Conclusion:

The "possible" correction to the calculated change in PZR level contained in Table II of my Transmittal package 86-2226-00 is displayed below:

Date of Rx Trip	Measured Change in PZR level Inches	Time to Minimum PZR Level sec	Calculated PZR level Change	Correction to Calc. PZR Level
2/24/78	191	60	184	-8.3 (176)
4/2/78	162	45	167	-8.2 (159)
8/2/78	196	90	206	-22.9 (183)
11/29/78	184	240	181	-14.7 (166)

Though the original assumption is too simple by assuming no change in RC system mass, the careful attention to recorded flowrates and net volume added to the RC system does not appear to add accuracy to the mathematical technique. Possible causes of error in this corrective method includes the following:

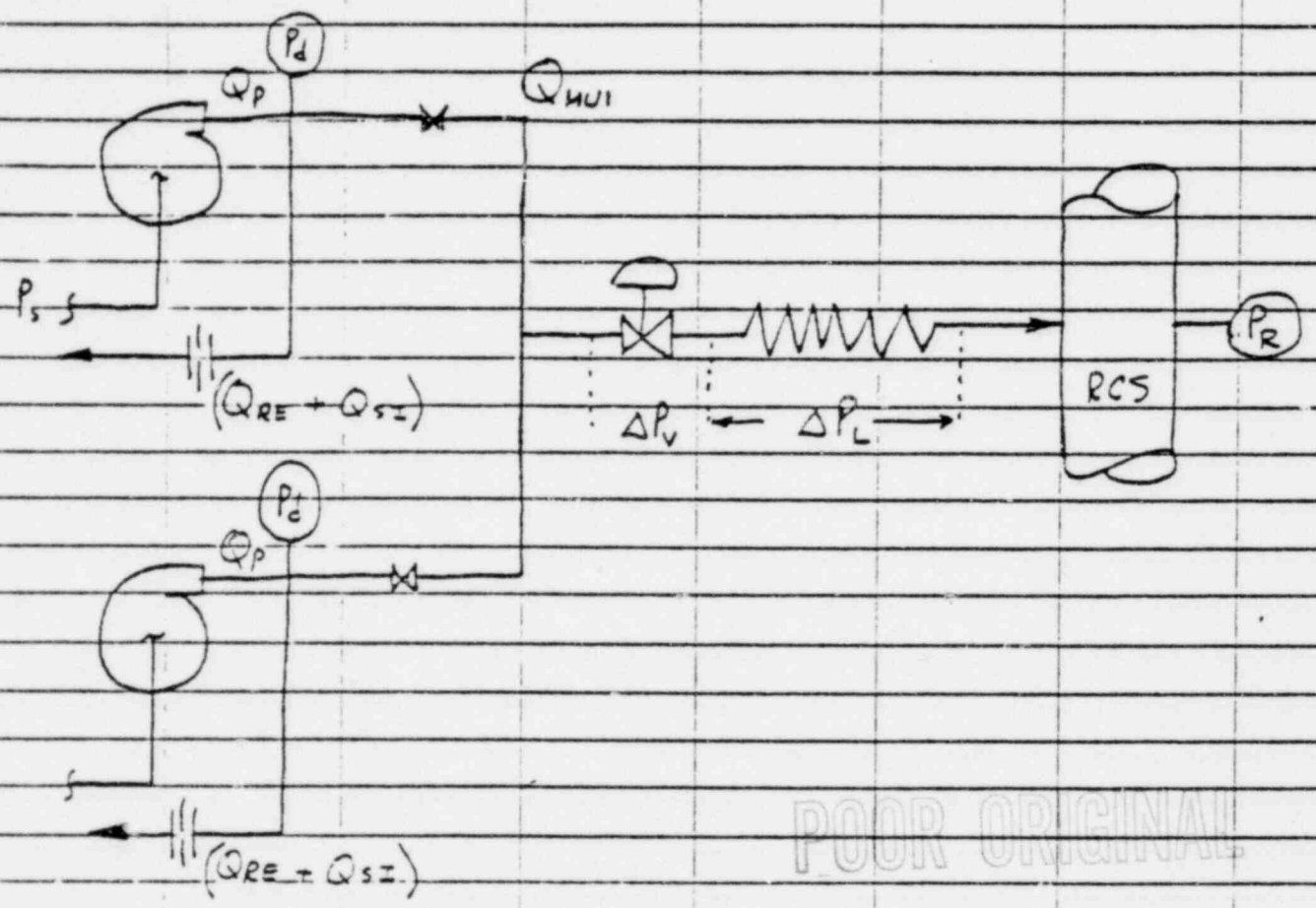
- (1) The Post Trip Review log contains updated data once every 30 seconds which is insufficient to accurately define flowrates during the nominal 60 second transient
- (2) The unmeasured total makeup flowrate into the RC system is based on calculated values which have not been confirmed and could lead to significant errors in estimating the net change to Pressurizer level.

STOWER <u>TECO</u> SUBJECT <u>PZR Level Due To Make Up Flow</u> CONT NO <u>86-2226-14</u> CALC BY <u>R. W. Winks</u> CHECK BY _____	PROP NO _____ DWG NO _____ GROUP NO _____ DATE <u>10/3/78</u> DATE _____
FILE NO _____ COMP NO _____ SHEET NO <u>15 of 22</u>	

POOR ORIGINAL

Calculation of Make Up System Performance

System Schematic



POOR ORIGINAL

$$P_d = P_R + \Delta P_v + \Delta P_L ; \quad Q_p = Q_{RE} + Q_{MU}$$

$$(P_d - P_s) = (P_R - P_s) + \Delta P_{sys} = \Delta P_{pump}$$

$$\Delta P_p (f Q_p) = (P_R - P_s) + \Delta P_{sys} (f Q_{MU})$$

Assume $Q_{RE} + Q_{SI} \approx 70$ gpm constant

$$\Delta P_p (f Q_{MU} + 70) = (P_R - P_s) + \Delta P_{sys} (f Q_{MU})$$

For 1#2 MU Pump Operation let RC pressure vary from 2200 psig down to 1200 psig
Use the DB-1 MU Pump H-Q curve.

Let $P_s \approx 15$ psig

MAKE UP
32-9745 00

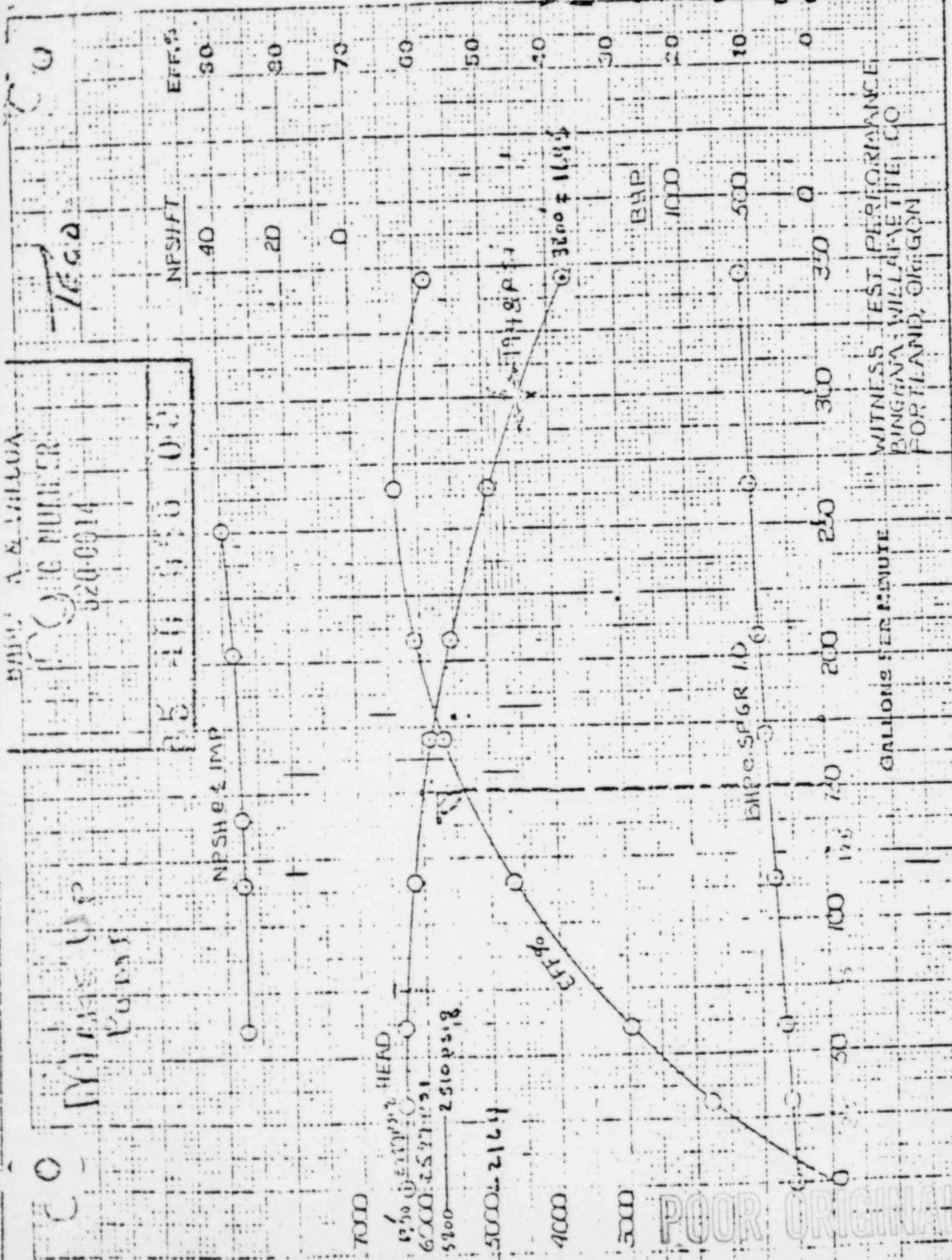
Page 17 of 22

BABCOCK & WILCOX
PUMP CURVE NUMBER
320-0014

WILCOX PUMPS

TEC-0

2X3X7 1/2 CP



WITNESS TEST PERFORMANCE
BINGHAM WILLAMETTE CO
PORTLAND, OREGON

IMPPELLER
MAX DIA 7 1/2
MIN DIA 7 3/16
CYE C, A, B, C, D, E, F, G, H, I, J, K, L, M, N, O, P, Q, R, S, T, U, V, W, X, Y, Z, AA, AB, AC, AD, AE, AF, AG, AH, AI, AJ, AK, AL, AM, AN, AO, AP, AQ, AR, AS, AT, AU, AV, AW, AX, AY, AZ, BA, BB, BC, BD, BE, BF, BG, BH, BI, BJ, BK, BL, BM, BN, BO, BP, BQ, BR, BS, BT, BU, BV, BW, BX, BY, BZ, CA, CB, CC, CD, CE, CF, CG, CH, CI, CJ, CK, CL, CM, CN, CO, CP, CQ, CR, CS, CT, CU, CV, CW, CX, CY, CZ, DA, DB, DC, DD, DE, DF, DG, DH, DI, DJ, DK, DL, DM, DN, DO, DP, DQ, DR, DS, DT, DU, DV, DW, DX, DY, DZ, EA, EB, EC, ED, EE, EF, EG, EH, EI, EJ, EK, EL, EM, EN, EO, EP, EQ, ER, ES, ET, EU, EV, EW, EX, EY, EZ, FA, FB, FC, FD, FE, FF, FG, FH, FI, FJ, FK, FL, FM, FN, FO, FP, FQ, FR, FS, FT, FU, FV, FW, FX, FY, FZ, GA, GB, GC, GD, GE, GF, GG, GH, GI, GJ, GK, GL, GM, GN, GO, GP, GQ, GR, GS, GT, GU, GV, GW, GX, GY, GZ, HA, HB, HC, HD, HE, HF, HG, HH, HI, HJ, HK, HL, HM, HN, HO, HP, HQ, HR, HS, HT, HU, HV, HW, HX, HY, HZ, IA, IB, IC, ID, IE, IF, IG, IH, II, IJ, IK, IL, IM, IN, IO, IP, IQ, IR, IS, IT, IU, IV, IW, IX, IY, IZ, JA, JB, JC, JD, JE, JF, JG, JH, JI, JJ, JK, JL, JM, JN, JO, JP, JQ, JR, JS, JT, JU, JV, JW, JX, JY, JZ, KA, KB, KC, KD, KE, KF, KG, KH, KI, KJ, KK, KL, KM, KN, KO, KP, KQ, KR, KS, KT, KU, KV, KW, KX, KY, KZ, LA, LB, LC, LD, LE, LF, LG, LH, LI, LJ, LK, LL, LM, LN, LO, LP, LQ, LR, LS, LT, LU, LV, LW, LX, LY, LZ, MA, MB, MC, MD, ME, MF, MG, MH, MI, MJ, MK, ML, MM, MN, MO, MP, MQ, MR, MS, MT, MU, MV, MW, MX, MY, MZ, NA, NB, NC, ND, NE, NF, NG, NH, NI, NJ, NK, NL, NM, NN, NO, NP, NQ, NR, NS, NT, NU, NV, NW, NX, NY, NZ, OA, OB, OC, OD, OE, OF, OG, OH, OI, OJ, OK, OL, OM, ON, OO, OP, OQ, OR, OS, OT, OU, OV, OW, OX, OY, OZ, PA, PB, PC, PD, PE, PF, PG, PH, PI, PJ, PK, PL, PM, PN, PO, PP, PQ, PR, PS, PT, PU, PV, PW, PX, PY, PZ, QA, QB, QC, QD, QE, QF, QG, QH, QI, QJ, QK, QL, QM, QN, QO, QP, QQ, QR, QS, QT, QU, QV, QW, QX, QY, QZ, RA, RB, RC, RD, RE, RF, RG, RH, RI, RJ, RK, RL, RM, RN, RO, RP, RQ, RR, RS, RT, RU, RV, RW, RX, RY, RZ, SA, SB, SC, SD, SE, SF, SG, SH, SI, SJ, SK, SL, SM, SN, SO, SP, SQ, SR, SS, ST, SU, SV, SW, SX, SY, SZ, TA, TB, TC, TD, TE, TF, TG, TH, TI, TJ, TK, TL, TM, TN, TO, TP, TQ, TR, TS, TT, TU, TV, TW, TX, TY, TZ, UA, UB, UC, UD, UE, UF, UG, UH, UI, UJ, UK, UL, UM, UN, UO, UP, UQ, UR, US, UT, UY, UZ, VA, VB, VC, VD, VE, VF, VG, VH, VI, VJ, VK, VL, VM, VN, VO, VP, VQ, VR, VS, VT, VU, VV, VW, VX, VY, VZ, WA, WB, WC, WD, WE, WF, WG, WH, WI, WJ, WK, WL, WM, WN, WO, WP, WQ, WR, WS, WT, WU, WV, WW, WX, WY, WZ, XA, XB, XC, XD, XE, XF, XG, XH, XI, XJ, XK, XL, XM, XN, XO, XP, XQ, XR, XS, XT, XU, XV, XW, XX, XY, XZ, YA, YB, YC, YD, YE, YF, YG, YH, YI, YJ, YK, YL, YM, YN, YO, YP, YQ, YR, YS, YT, YU, YV, YW, YX, YY, YZ, ZA, ZB, ZC, ZD, ZE, ZF, ZG, ZH, ZI, ZJ, ZK, ZL, ZM, ZN, ZO, ZP, ZQ, ZR, ZS, ZT, ZU, ZV, ZW, ZX, ZY, ZZ

CHARACTERISTIC CURVE SHEET
BINGHAM PUMP DIVISION
BINGHAM-WILLAMETTE COMPANY

THE BABCOCK & WILCOX CO
TOLEDO EDISON CO
DO NOT SEAL INTERSECTION

POOR ORIGINAL

32-9745 00

M.U. PUMP DISCHARGE PRESSURE VERSUS PUMP FLOWRATE
FOR DAVIS-BESSE 1

NOTE:

FLUID TEMPERATURE = 100 F

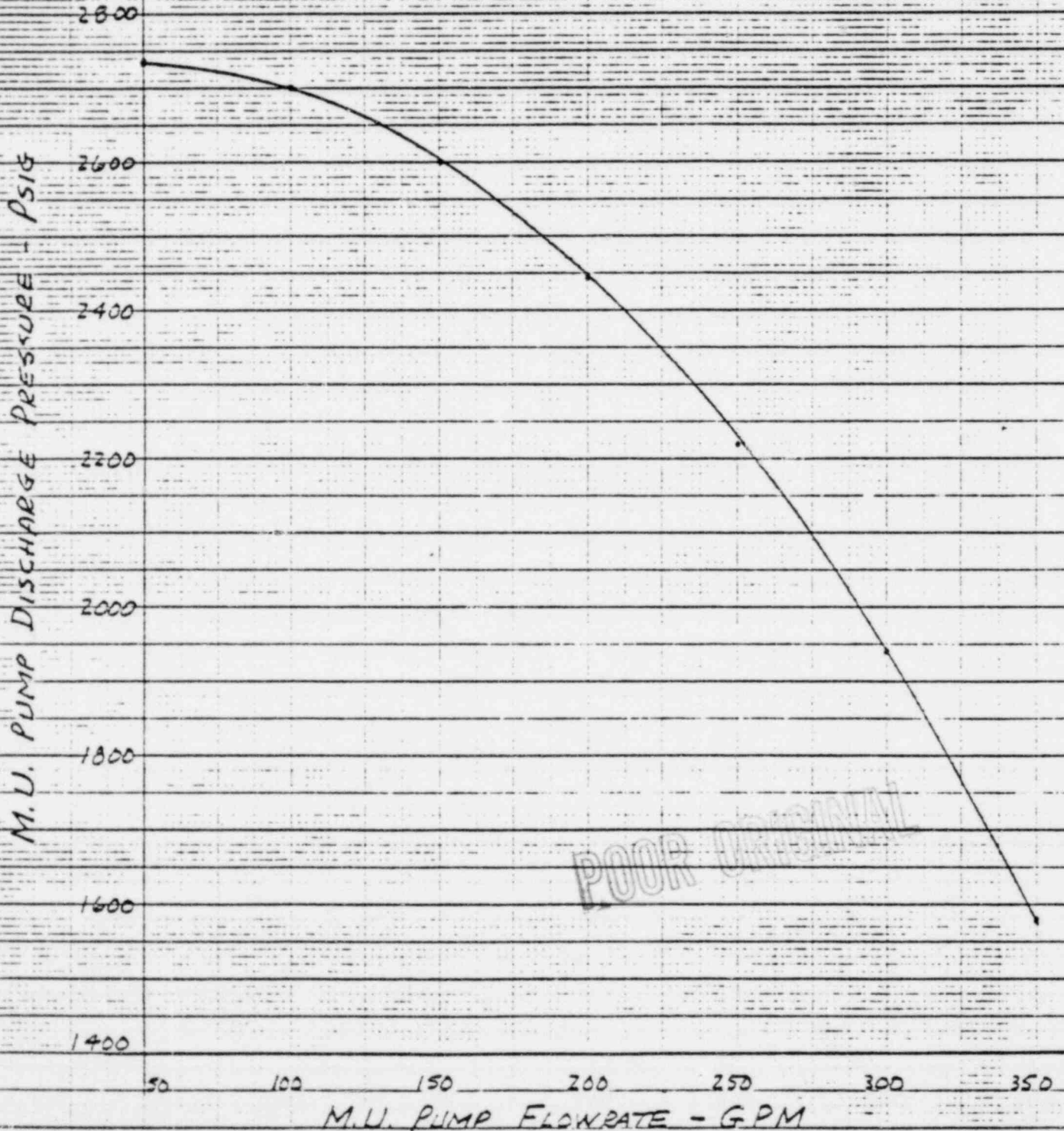


FIG 5

46 1470

IN. K. M. E. D. S. B. E. R. A. S. T. S. O. B. S. E. R. V. E. S.
P. L. A. N. E. T. S. & P. R. O. J. E. C. T. S. M. A. D. E. I. N. U. S. A.

POOR ORIGINAL

32-9745 00

1 MW Pump Operation:
 $k_1 = 0.010$ and 0.0050
 = (psid/gpm²)

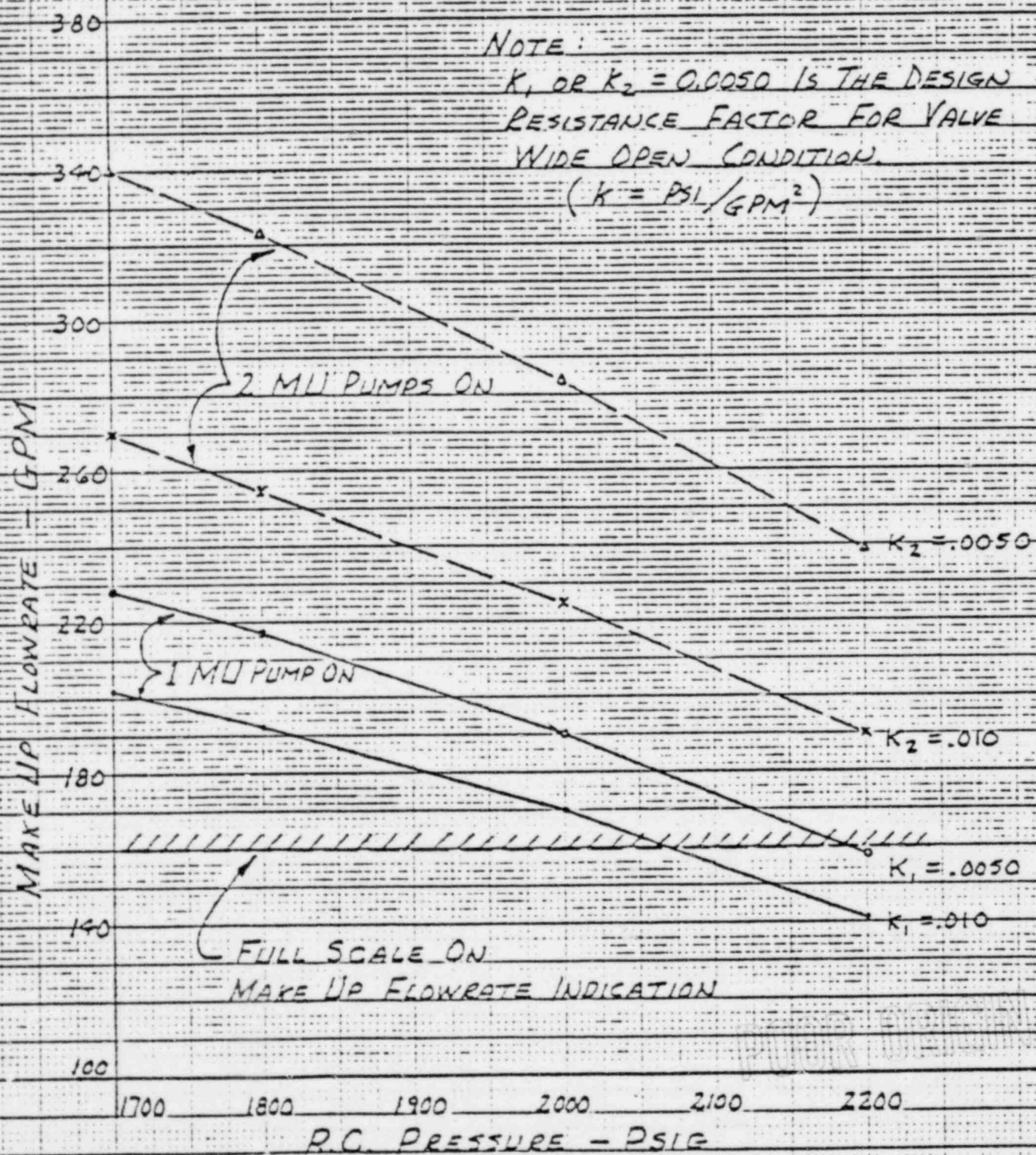
Pre psig	Q _{MU} gpm	Q _{RESI} gpm	Q _{pump} gpm	Pd psig	ΔP _{sys} psi	k ₁	Q _{MU'} gpm
2200	142	70	212	2400	200	0.010	141
2000	169	70	239	2290	290	.010	170
1800	192	70	262	2169	369	.010	192
1700	203	70	273	2108	408	.010	202
2200	160	70	230	2325	125	.0050	158
2000	190	70	260	2180	180	.0050	190
1800	215	70	285	2036	236	.0050	217
1700	227	70	297	1960	260	.0050	228

2 MW Pump Operation with same system Resistance
 $k_2 = k_1 = 0.010$ and 0.0050 psi/gpm²

Pre	Q _{MU}	Q _{PUMP}	Q _{TOT}	Pd	ΔP _{sys}	k ₁	Q _{TOT'}
2200	95	165	190	2562	362	.010	190
2000	112.5	182.5	225	2508	508	.010	225
1800	127.5	197.5	255	2456	656	.010	256
1700	135	205	270	2430	730	.010	270
2200	119	189	238	2485	285	.0050	239
2000	142	212	284	2402	402	.0050	284
1800	161	231	322	2322	522	.0050	323
1700	170	240	340	2280	580	.0050	340

POOR ORIGINAL

CALCULATED MAKEUP FLOWRATES FOR EITHER 1 OR 2 MAKE UP PUMPS VERSUS R.C. PRESSURE AT DAVIS-BESSE 1

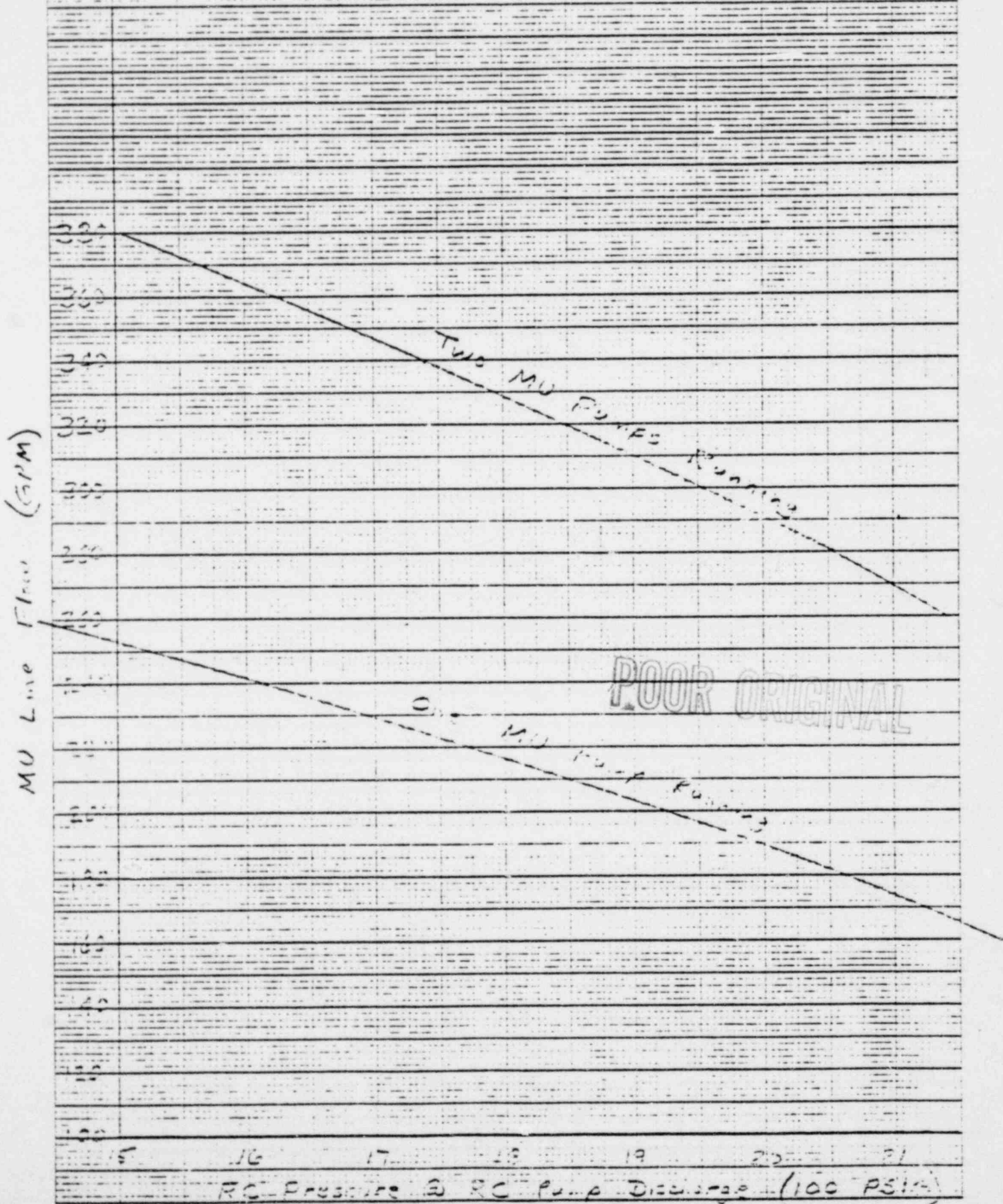


46 1470

K-E 10 X 10 TO 1/2 INCHES 715 X 10 INCHES KLUFFEL & ESSER CO. MADE IN U.S.A.

FIG 6

CALCULATED H.U. SYSTEM FLOWRATE VERSUS RC PRESSURE
FOR VALVE WIDE OPEN CONDITIONS



46 1320

16 X 10 TO 1/2 INCH 7 X 10 INCHES
RUFFEL & ESSER CO. NEW YORK

TEST DATA CALCULATIONS

(1)	(2)	(3)	(4)	(5)	(6)	(7)
Flow (GPM)	MV Line Flow (GPM)	(2) + (3) (GPM)	MV Line ΔP (PSI)	MV Pump TCH (PSI)	PS Pump ΔP (PSI)	HPI Nozzle
						MV Line ΔP = 67.44 PSI @ 114 GPM (value wide open)
						$k = .0052 \text{ psi/gpm}^2$
32	100	100	102	2400	2200	
32	150	182	117	2355	2200	
32	160	197	122	2315	2185	
32	180	212	136	2280	2062	
32	200	232	203	2130	1911	
32	220	252	251	2015	1772	
32	240	272	299	1915	1613	
32	260	292	351	1790	1439	
		(4) + (5)				
32	160	96	133	2320	2297	
32	200	120	202	2270	2177	
32	240	136	299	2220	2057	
32	280	152	407	2160	2038	
32	320	168	531	2100	1919	
32	360	184	673	2040	1800	
32	400	196	827	1980	1681	
32	330	206	1000	2055	1500	
32	370	231	710	2290	1570	
32	410	256	537	2420	1450	
32	340	186	600	2340	1740	
32	260	146	351	2490	2139	

POOR ORIGINAL

TECO
Appendix to 32-9745-00

14
J.R. Merchant for
R.W. Winks

10/3/78