

**CALCULATION OF RELEASES
OF RADIOACTIVE MATERIALS
IN GASEOUS AND LIQUID EFFLUENTS
FROM BOILING WATER REACTORS
(BWR-GALE CODE)**

April 1976



**Office of Standards Development
U. S. Nuclear Regulatory Commission**

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CHAPTER 1. BWR-GALE CODE

1.1 INTRODUCTION

The BWR-GALE (Boiling Water Reactor Gaseous and Liquid Effluents) Code is a computerized mathematical model for calculating the release of radioactive material in gaseous and liquid effluents from boiling water reactors (BWRs). The calculations are based on data generated from operating reactors, field tests, laboratory tests, and plant-specific design considerations incorporated to reduce the quantity of radioactive materials that may be released to the environment.

The average quantity of radioactive material released to the environment from a nuclear power reactor during normal operation is called the "source term," since it is the source or initial number used in calculating the environmental impact of radioactive releases. The calculations performed by the BWR-GALE Code are based on (1) standardized primary and secondary coolant activities derived from American Nuclear Society (ANS) 18.1 Working Group recommendations (Ref. 1), (2) release and transport mechanisms that result in the appearance of radioactive material in liquid and gaseous waste streams, and (3) plant-specific design features used to reduce the quantities of radioactive materials ultimately released to the environs.

In a BWR, water is converted to steam by heat from the fuel elements in the reactor. The steam expands through a turbine and then is condensed and returned to the reactor. The principal mechanisms that affect the concentrations of radioactive materials in the reactor coolant are (1) fission product leakage to the coolant from defects in the fuel cladding and fission product generation in tramp uranium, (2) corrosion products activated in the core, (3) radioactivity removed by the reactor coolant cleanup system, (4) radioactivity removed by the condensate demineralizers, (5) radioactivity removed through the steam-jet ejectors, and (6) radioactivity removed due to reactor coolant leakage. These mechanisms are described briefly in the following paragraphs.

Fission products enter the coolant as a result of defects in the fuel cladding and from the tramp uranium on the cladding surfaces, while corrosion products are activated in the reactor core. These impurities must be continuously removed from the reactor coolant to prevent damage to the fuel elements and other reactor components. The removal is accomplished in two ways: (1) after passing through the turbine, the condensed steam is processed through the condensate cleanup system (e.g., demineralizers) and returned to the reactor for reuse and (2) a side stream of reactor coolant is continuously withdrawn, processed through the reactor cleanup system (demineralizers), and returned to the reactor vessel. Both cleanup systems remove particulates and ionic impurities from the reactor coolant. The materials collected by the demineralizers are removed periodically by chemical regeneration or by replacement of resins. The liquid wastes are processed in the liquid waste treatment system, and the spent ion exchange resins are transferred to the solid waste treatment system and prepared for offsite shipment.

Radioactive gases are removed from the condensing steam in the main condenser by the steam-jet air ejectors. This source of gaseous waste is treated principally by delaying the release to permit radioactive decay. Alternative treatment methods include holdup lines, long-term holdup systems using charcoal delay systems, and cryogenic distillation.

Another potential release point of radioactive material is the exhaust from the turbine gland sealing system. A sidestream of primary steam flows through the turbine gland seal. The steam is condensed and returned to the condenser hotwell for reuse in the reactor. However, noble gases, activation gases, radioactive particulates, and iodine that remain in the gaseous phase must be vented. The treatment provided this source of gaseous waste is normally a two-minute holdup line that permits decay of the short-lived noble and activation gases before they are released to the environment. Clean steam (nonradioactive steam) may be used in place of primary steam to eliminate the gland seal as an activity release point.

Following plant shutdowns, mechanical vacuum pumps are used to reestablish the main condenser vacuum. In addition, the mechanical vacuum pumps may be used during plant shutdowns to maintain a slight condenser vacuum and thereby prevent outleakage of gases from the main condenser. If required to meet the design objectives of Appendix I, the effluent from the mechanical vacuum pump could be processed through charcoal adsorbers for removal of radioiodine prior to release.

In addition to the above release points, the BWR-GALE Code, the calculational model used for BWR source term calculations, considers releases from the turbine, containment, auxiliary, and radwaste buildings due to leakage from contaminated systems. Such leakage from systems containing main steam or reactor coolant may have an appreciable effect on the radioactive source term. Leakage may occur through valve stems, pump seals, and flanged connections. The amount of airborne radioactive material released is a function of reactor coolant temperature, pressure, and activity at the point where the leak occurs. Included with the leaking steam or coolant are noble gases, iodine, and particulates that are released directly to the building atmosphere. In some cases, leakage may be reduced by special design features such as vacuum leakoff drains or "clean" steam on the valve bonnets in addition to normal precautions such as backseating valves and using all-welded systems. Leakage can also be reduced by the use of closed leakoff drains and by increased maintenance.

Liquid waste sources include liquid streams used to sluice (transfer), backwash, regenerate, and rinse demineralizer resins; laundry waste water; personnel shower wastes; laboratory drain wastes; decontamination wastes; and water collected in equipment drains and floor drains.

This chapter provides a step-by-step explanation of the BWR-GALE Code and a description of the parameters that have been built into the Code for use with all BWR source term calculations. These parameters, which apply generically to all BWRs, have been incorporated into the Code to eliminate the need for their entry on input data cards. This chapter also describes the entries required to be entered on input data cards used by the Code. Explanations of the data required, along with acceptable means for calculating such data, are given for each input data card. Chapter 2 gives the principal source term parameters developed for use with the BWR-GALE Code and explains the bases for each parameter. Chapter 3 contains a sample data input sheet and a FORTRAN listing of the BWR-GALE Code. Chapter 4 lists the information needed to generate source terms that an applicant is required to submit with the application.

1.2 DEFINITIONS

The following definitions apply to terms used in this report:

Activation Gases: The gases (including oxygen, nitrogen, and argon) that become radioactive due to irradiation in the core.

Chemical Waste Stream: Normally liquids that contain relatively high concentrations of decontamination wastes or chemical compounds other than detergents. These liquids originate primarily from resin regenerants and laboratory waste.

Decontamination Factor (DF): The ratio of the initial amount of a nuclide in a stream (specified in terms of concentration or activity of radioactive materials) to the final amount of that nuclide in a stream following treatment by a given process.

Detergent Waste Stream: Liquids that contain detergent, soaps, or similar organic materials. These liquids consist principally of laundry, personnel shower, and equipment decontamination wastes and normally have a low radioactivity content.

Effective Full Power Days: The number of days a plant would have to operate at 100% licensed power to produce the integrated thermal power output during a calendar year; i.e.,

$$\text{Effective Full Power Days} = \frac{\text{Integrated Thermal Power}}{\text{Licensed Power Level}} = \frac{EP_i T_i}{P_{\text{total}}}$$

where

P_i is the i th power level, in Mwt;

P_{total} is the license power level, in Mwt; and

T_i is the time of operation at power level i , in days.

Fission Product: A nuclide produced either by fission or by subsequent radioactive decay or neutron activation of the nuclides formed in the fission process.

Gaseous Effluent Stream: Processed gaseous waste containing radioactive materials resulting from the operation of a nuclear power reactor.

High-Purity Waste Stream: Liquids, normally of low conductivity, consisting primarily of liquid waste collected from building equipment drains, valve and pump seal leakoffs, demineralizer backwash, ultrasonic resin cleaning, and resin transfer. These liquids are normally reused as primary coolant makeup water after processing.

Liquid Effluent Stream: Processed liquid wastes containing radioactive materials resulting from the operation of a nuclear power reactor.

Low-Purity Waste Stream: Liquids, normally of high conductivity and not of primary quality, collected from building sumps, uncollected valve and pump seal leakoffs, miscellaneous vents, and floor drains.

Partition Coefficient (PC): The ratio of the concentration of a nuclide in the gas phase to the concentration of that nuclide in the liquid phase when the liquid and gas are at equilibrium.

Partition Factor (PF): The ratio of the quantity of a nuclide in the gas phase to the total quantity in both the liquid and gas phases when the liquid and gas are at equilibrium.

Plant Capacity Factor: The ratio of the average net power to the rated power capacity.

Radioactive Halogens: The isotopes of fluorine, chlorine, bromine, and iodine. The radioactive isotopes of iodine are the key isotopes considered in dose calculations.

Radioactive Noble Gases: The radioactive isotopes of helium, neon, argon, krypton, xenon, and radon, which are characterized by their chemical inactivity. The radioactive isotopes of krypton and xenon are the key elements considered in dose calculations.

Radioactive Release Rate: The average quantity of radioactive material released to the environment from a nuclear power reactor during normal operation including anticipated operational occurrences.

Reactor Coolant (Primary Coolant): The fluid circulated through the reactor to remove heat. In a BWR, the fluid allowed to boil in the reactor vessel to generate steam and power the turbine. The reactor coolant activity is considered to be constant over a range of power levels, coolant and cleanup flows, and reactor coolant volumes. The radionuclide distributions and concentrations for the reactor coolant and main steam are based on the values proposed in the ANS T8.1 (Ref. 1) Working Group draft standard for BWRs. Provisions are made in the BWR-GALE Code, in accordance with the recommendations of the draft standard, for adjusting reactor coolant concentrations should the plant be designed to parameters that are outside the ranges considered in the standard. The radionuclide concentrations used are representative of measured values based on the available data. The radionuclides are divided into the following categories:

1. Noble gases
2. Halogens (Br, I)
3. Cesium and Rubidium
4. Water activation products
5. Other nuclides (as listed in Table 2-2 of Chapter 2 of this document)

Regenerant Solutions Waste Stream: Liquids containing regeneration chemical compounds that originate from regeneration of the condensate demineralizer resins.

Source Term: The calculated average quantity of radioactive material released to the environment from a nuclear power reactor during normal operation including anticipated operational occurrences. The source term is the isotopic distribution of radioactive materials used in evaluating the impact of radioactive releases on the environment.

Tramp Uranium: The uranium present on the cladding of a fuel rod.

1.3 GASEOUS SOURCE TERMS

The following sources are considered in calculating the release of radioactive materials (noble gases, radioactive particulates, and iodine) in gaseous effluents from normal operation including anticipated operational occurrences:

1. Main condenser offgas system,
2. Turbine gland sealing system,
3. Mechanical vacuum pumps, and
4. Ventilation exhaust air from the containment, auxiliary, radwaste, and turbine buildings.

The releases of radioactive materials in ventilation exhaust air from buildings not covered in 4. above are calculated to be negligible when compared to the gaseous source term from the sources listed above and are therefore not considered individually in the source term calculations.

Calculations show that approximately 9.5 Ci/yr of carbon-14 will be released from a BWR. All carbon-14 releases are assumed to be in the form of a vapor from the main condenser evacuation system vent.

Argon-41 is formed in the drywell by neutron activation of stable, naturally occurring argon-40 in the drywell air. The argon-41 is released to the environment when the drywell is vented or purged. Based on releases reported by licensees in semiannual reports, it is expected that, independent of power level, approximately 25 Ci/yr of argon-41 will be released to the environment.

The releases of radioactive materials in gaseous effluents are based on measurements made at operating BWRs. The radiiodine, radioactive particulate, and noble gas release rates are specified in the BWR-GALE Code and are modified only as needed to reflect treatment processes. Gaseous releases for building ventilation exhaust systems and the main condenser offgas system are based on the average of actual measurements.

The BWR-GALE Code also calculates tritium releases through the ventilation exhaust systems. The annual quantity of tritium available for release is calculated using a functional relationship derived from measured liquid and vapor tritium releases at operating BWRs and considering the integrated thermal power output during the calendar year in which the releases occurred. This relationship expresses total tritium as a function of power output. The tritium releases through the ventilation exhaust systems are assumed to be the total tritium available for release minus the tritium calculated to be released through the liquid pathway. Except for tritium, the radioactivity released in ventilation air is considered to be independent of the power level. Releases from the mechanical vacuum pump are also considered to be independent of the power level.

Chapter 2 provides iodine and particulate decontamination factors for removal equipment and parameters for calculating holdup times for noble gases and for calculating tritium releases.

1.4 LIQUID SOURCE TERMS

The following sources are considered in calculating the release of radioactive materials in liquid effluents from normal operations including anticipated operational occurrences:

1. Processed liquid wastes from the high-purity waste system,
2. Processed liquid wastes from the low-purity waste system,
3. Processed liquid wastes from the chemical waste system,
4. Processed liquid regenerant wastes, and
5. Detergent wastes.

The radioactivity input to the liquid radwaste treatment system is based on flow rates of the liquid waste streams and their radioactivity levels, expressed as a fraction of the primary reactor coolant activity (PCA). The primary coolant activity (PCA) is based on the recommendations of the ANS 18.1 Working Group (Ref. 1), which considers a noble gas release rate of 60,000 $\mu\text{Ci/sec}$ after a 30-minute decay.

Radionuclide removal by the liquid radwaste treatment system is based on the following parameters:

1. Decay during collection and processing and
2. Removal by the proposed treatment systems, e.g., filtration, ion exchange, evaporation, reverse osmosis, and plateout.

For BWRs using a deep-bed condensate demineralizer, the inventory of radionuclides collected on the demineralizer resins is calculated by considering the flow rate of condensate at main steam activity that is processed through the demineralizers and radionuclide removal using the decontamination factors given in Chapter 2. The radioactivity content of the demineralizer regenerator solution is obtained by considering that all of the activity is removed from the resins at the interval dictated by the regeneration frequency.

Methods for calculating collection and processing times and the decontamination factors for radwaste treatment equipment are given in this chapter. The liquid radioactive source terms are adjusted to compensate for equipment downtime and anticipated operational occurrences.

For plants having an onsite laundry, a standard detergent source term, adjusted for the treatment provided, is added to the adjusted source term.

1.5 INSTRUCTIONS FOR COMPLETING BWR-GALE CODE INPUT DATA CARDS

1.5.1 PARAMETERS INCLUDED IN THE BWR-GALE CODE

The parameters listed below are built into the BWR-GALE Code since they are generally applicable to all BWR source term calculations and do not require entry on input data cards.

1.5.1.1 Plant Capacity Factor

0.80 (292 effective full power days per year).

1.5.1.2 Radionuclide Concentrations in the Reactor Coolant and Main Steam

See Chapter 2, Tables 2-2 through 2-5 of this document.

1.5.1.3 Noble Gas, Iodine, and Particulate Releases From Building Ventilation Systems Prior to Treatment

See Table 1-1.

1.5.1.4 Radioiodine Input Rate to Main Condenser Offgas System

5 Ci/yr per reactor downstream of main condenser air ejectors.

1.5.1.5 Main Condenser Vacuum Pump Release

Xe-133 -- 2300 Ci/yr

Xe-135 -- 350 Ci/yr

I-131 -- 0.03 Ci/yr

1.5.1.6 Charcoal Delay Systems

For a charcoal delay system used to treat the offgases from the main condenser air ejector, the BWR-GALE Code calculates the holdup times for Kr and Xe. Iodine releases from charcoal delay systems are negligible due to the large quantities of charcoal used in the system. The holdup times for noble gases are calculated by the Code using the following equation, and the data are entered on Cards 31-35.

$$T = 0.262 \frac{MK}{TO/N}$$

TABLE 1-1
 RELEASES FROM BUILDING VENTILATION SYSTEMS PRIOR TO TREATMENT
 (in Ci/yr per Reactor)

<u>NUCLIDE</u>	<u>CONTAINMENT BUILDING</u>	<u>AUXILIARY BUILDING</u>	<u>TURBINE* BUILDING</u>	<u>RADWASTE BUILDING</u>
Kr-83m	**	**	**	**
Kr-85m	3	3	68	**
Kr-85	**	**	**	**
Kr-87	3	3	190	**
Kr-88	3	3	230	**
Kr-89	**	**	**	**
Xe-131m	**	**	**	**
Xe-133m	**	**	**	**
Xe-133	66	66	280	10
Xe-135m	46	46	650	**
Xe-135	34	34	630	45
Xe-137	**	**	**	**
Xe-138	7	7	1440	**
I-131	0.17	0.17	0.19	0.046
I-133	0.68	0.68	0.76	0.18
Co-60	0.01	0.01	0.002	0.09
Co-58	0.0006	0.0006	0.0006	0.0045
Cr-51	0.0003	0.0003	0.013	0.009
Mn-54	0.003	0.003	0.0006	0.036
Fe-59	0.0004	0.0004	0.0005	0.015
Zn-65	0.002	0.002	0.0002	0.001
Zr-95	0.0004	0.0004	0.0001	0.00005
Sr-89	0.00009	0.00009	0.006	0.0005
Sr-90	0.000005	0.000005	0.00002	0.0003
Sb-124	0.0002	0.0002	0.0003	0.00005
Cs-134	0.004	0.004	0.0003	0.0045
Cs-136	0.0003	0.0003	0.0005	0.00045
Cs-137	0.005	0.005	0.0006	0.009
Ba-140	0.0004	0.0004	0.011	0.0001
Ce-141	0.0001	0.0001	0.0006	0.0026

*For special design feature to control leakage from valves in lines 2-1/2 inches and larger, reduce the turbine building leakage rates by a factor of five.

**Less than 1 Ci/yr per reactor for noble gases.

where

K is the dynamic adsorption coefficient, in cm^3/g ,

M is the mass of charcoal, in 10^3 lb ,

T is the holdup time, in hr, and

$10 N$ is the number of condenser shells times 10, in ft^3/min per shell.

1.5.1.7 Cryogenic Distillation System

For a cryogenic distillation system, the BWR-GALE Code uses a partition factor (PF) of 0.0001 for Xe and I and a PF of 0.00025 for Kr to calculate Xe, I, and Kr losses during separation by distillation. The Xe, I, and Kr separated by distillation are considered to be released following 90-day holdup. The calculated releases are the sum total of the noble gases and iodine released from the overheads during distillation without holdup and the noble gases and iodine released following 90-day holdup.

1.5.1.8 Decontamination Factors for Condensate Demineralizers

Demineralizer	Halogens	Cs, Ru	Other Nuclides
Deep bed	10	2	10
Powdex	10	2	10

Note: For a system using filter/demineralizers (Pwdx), a zero is entered for regeneration frequency on Card 6, as explained later in Section 1.5.2.6.

1.5.1.9 Detergent Wastes

The radionuclides listed in Table 2-32 of Chapter 2 are assumed to be released unless treatment is provided or laundry is not processed on site.

1.5.1.10 Tritium Releases

Total tritium release equals 0.025 Ci/yr per Mwt. The quantity of tritium released through the liquid pathway is the calculated annual volumetric liquid release times 0.01 $\mu\text{Ci}/\text{ml}$ of tritium in liquid waste. The difference between the total release and liquid release is the amount considered to be released through the plant ventilation exhaust systems.

1.5.1.11 Regeneration of Condensate Demineralizers

Flow rates and concentrations of radioactive materials routed to the liquid radwaste system from the chemical regeneration of the condensate demineralizers are based on the following parameters:

1. Liquid flow to the demineralizer is based on the radioactivity of the main steam.
2. All radionuclides removed from the condensate by the demineralizers are removed from the demineralizer resins during chemical regeneration. The regenerant waste radioactivity is adjusted for radionuclide decay during operation of the demineralizers.
3. The radioactivity in the regenerant wastes is adjusted for radionuclide decay on the resins during demineralizer operation.

1.5.1.12 Adjustment to Liquid Radwaste Source Terms for Anticipated Operational Occurrences

1. The calculated source term is increased by 0.15 Ci/yr per reactor using the same isotopic distribution as for the calculated source term to account for anticipated occurrences such as operator errors resulting in unplanned releases.

2. Evaporators are assumed to be unavailable for two consecutive days per week for maintenance. If a two-day holdup capacity or an alternative evaporator is available, no adjustment is needed. If less than a two-day capacity is available, the waste excess is assumed to be handled as follows:

- a. High-Purity or Low-Purity Waste--Processed through an alternative system (if available) using a discharge fraction consistent with the lower purity system.
- b. Chemical Waste--Discharged to the environment to the extent holdup capacity or an alternative evaporator is not available.

1.5.2 PARAMETERS REQUIRED FOR THE BWR-GALE CODE

The parameters described in the following sections must be entered on input data cards. Complete the cards designated below by "(SAR/ER)" from information given in the Safety Analysis and Environmental Reports. Complete the remaining cards (i.e., those not designated below as "(SAR/ER)" cards) using the principal source term parameters specified below and discussed in Chapter 2.

1.5.2.1 Card 1: Name of Reactor (SAR/ER)

Enter in spaces 33-60 the name of the reactor.

1.5.2.2 Card 2: Thermal Power Level (SAR/ER)

Enter in spaces 73-80 the maximum thermal power level (in MWt) evaluated for safety considerations in the Safety Analysis Report.

Note: Adjust all power-dependent parameters to this power level.

1.5.2.3 Card 3: Total Steam Flow Rate (SAR/ER)

Enter in spaces 73-80 the total steam flow rate from the reactor (in 10^6 lb/hr).

1.5.2.4 Card 4: Mass of Coolant in Reactor Vessel (SAR/ER)

Enter in spaces 73-80 the mass of water in the reactor vessel (in 10^6 lb).

1.5.2.5 Card 5: Cleanup Demineralizer Flow (SAR/ER)

Enter in spaces 73-80 the primary coolant flow rate (in 10^6 lb/hr) through the reactor coolant cleanup system demineralizers.

1.5.2.6 Card 6: Condensate Demineralizer Regeneration Time

For deep-bed condensate demineralizers, use a 3.5-day regeneration frequency. If ultrasonic resin cleaning is used, assume a 7-day regeneration frequency. Multiply the frequency by the number of demineralizers and enter the calculated number of days in spaces 73-80. For filter/demineralizers (Powdex), enter zeros in spaces 73-80.

1.5.2.7 Card 7: Fraction of Feedwater Through Condensate Demineralizer (SAR/ER)

Enter in spaces 73-80 the fraction of feedwater processed through the condensate demineralizers.

1.5.2.8 Card 8: Dilution Flow (SAR/ER)

Enter in spaces 73-80 the annual average flow rate of water (10^3 gal/min) used to dilute liquid waste discharged to the environment.

1.5.2.9 Cards 9-20: Liquid Radwaste Treatment System Input Parameters

Four liquid radwaste inlet streams are considered in the BWR-GALE Code:

1. High-Purity Waste, Cards 9-11
2. Low-Purity Waste, Cards 12-14
3. Chemical Waste, Cards 15-17
4. Regenerant Solutions Waste, Cards 18-20

Three input data cards are used to define the major parameters for each of the four waste streams. Essentially the same information is needed on the three input data cards used for each of the four streams. The instructions given in this section are applicable to all four waste streams, with the following exception: the inlet waste activity is not entered on Card 18 for the regenerant solutions wastes for systems using regenerable condensate demineralizers since that activity is calculated by the Code.

The entries required on the first card (9, 12, and 15) for the High-Purity, Low-Purity, and Chemical Waste Systems, respectively, are outlined below and described in more detail in Section 1.5.2.9.1.

1. Enter in spaces 18-41 the name of the waste inlet stream (e.g., high-purity wastes).
2. Enter in spaces 42-49 the flow rate (in gal/day) of the inlet stream.
3. Enter in spaces 57-61 the activity of the inlet stream expressed as a fraction of the primary coolant activity (PCA).

On the first card for the Regenerate Solutions Waste System (i.e., Card 18), enter in spaces 73-80 the flow rate of the regenerant solutions waste inlet stream.

The second card (10, 13, 16, and 19) for each waste stream contains the overall system decontamination factors for three categories of radionuclides, as follows:

1. Enter in spaces 21-28 the DF for iodine.
2. Enter in spaces 34-41 the DF for cesium and rubidium.
3. Enter in spaces 47-54 the DF for other nuclides.

The following entries are required on the third card (11, 14, 17, and 20) for each waste stream:

1. Enter in spaces 29-33 the waste collection time (in days) prior to processing.
2. Enter in spaces 48-53 the waste processing and discharge time (in days).
3. Enter in spaces 72-77 the average fraction of wastes to be discharged after processing.

The following sections explain in more detail the use of the parameters in this document and the information given in the SAR/ER to make the data entries in Cards 9-20 listed above.

1.5.2.9.1 Liquid Waste Flow Rates and Activities (Cards 9, 12, 15, and 18)

Calculate flow rates and activities to complete the first card for each liquid radwaste inlet stream by using the waste volumes and activities given in Table 1-2. To the input flow rates given in the table, add expected flows and activities more specific to the plant design as given in the SAR/ER. The inlet streams should be combined to form the four principal waste streams (high-purity, low-purity, chemical wastes, and regenerant wastes) considered in this document. Calculate the primary coolant activity (PCA) of each of the four principal inlet streams by determining the weighted average activity of the composite stream entering the waste collection tanks. For example, if inlet streams A, B, and C enter the low-purity waste collector tank at average rates and PCA as listed below:

Stream A 1,000 gal/day at 0.01PCA

Stream B 2,000 gal/day at 0.1PCA

Stream C 500 gal/day at 1.0PCA

the composite A, B, C activity would be calculated as follows:

$$\frac{(1000 \text{ gal/day})(0.01\text{PCA}) + (2000 \text{ gal/day})(0.1\text{PCA}) + (500 \text{ gal/day})(1.0\text{PCA})}{(1000 \text{ gal/day} + 2000 \text{ gal/day} + 500 \text{ gal/day})} = 0.2\text{PCA}$$

The entries on Card 12 for this example would then be: spaces 18-41, "Low-Purity Waste"; spaces 42-49, "3500"; spaces 57-61, "0.2."

TABLE 1-2
BWR LIQUID WASTES

SOURCE	EXPECTED DAILY AVERAGE INPUT FLOW RATE (in gal/day)		FRACTION OF THE PRIMARY COOLANT ACTIVITY (PCA)
	PLANT WITH ULTRASONIC RESIN CLEANER	PLANT WITHOUT ULTRASONIC RESIN CLEANER	
<u>Equipment Drains</u>			
Drywell	3,400	3,400	1.00
Containment, auxiliary building, and fuel pool	3,720	3,720	0.01
Radwaste building	1,060	1,060	0.01
Turbine building	2,960	2,960	0.01
Ultrasonic resin cleaner	15,000	-	0.05
Resin rinse	2,500	5,000	0.002
Subtotal	28,640	16,140	-
<u>Floor Drains</u>			
Drywell	700	700	1.00
Containment, auxiliary building, and fuel pool	2,000	2,000	0.01
Radwaste building	1,000	1,000	0.01
Turbine building	2,000	2,000	0.01
Subtotal	5,700	5,700	-
Cleanup phase separator decant	640	640	0.002
Laundry drains	450	450	*
Lab drains	500	500	0.02
Regenerants**	1,700	3,400	***
Condensate demineralizer backwash†	-	8,100	2×10^{-6}
Chemical lab waste	100	100	0.02
Total	37,730	26,930	

* Listed in BWR-GALE Code; see Table 2-32.

** Deep-bed condensate demineralizers.

*** Calculated by BWR-GALE Code.

† Filter/demineralizer (Powdex) condensate demineralizers.

The input flows and activities are entered in units of gal/day and fraction of PCA, respectively.

1.5.2.9.2 Decontamination Factors for Equipment Used in the Liquid Radwaste Treatment System (Cards 10, 13, 16, and 19)

The decontamination factors (DFs) should be entered in the second card for each liquid radwaste inlet stream. The DFs represent the expected equipment performance averaged over the life of the plant, including downtime. The following factors are to be considered in calculating overall decontamination factors for the various systems.

1. DFs are categorized by one of the following types of radionuclides:

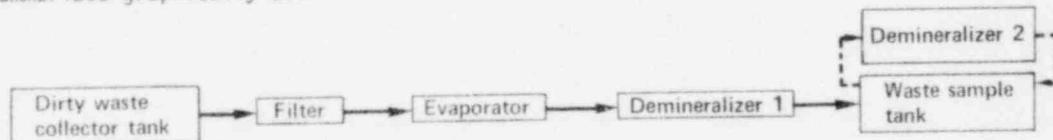
- a. Halogens
- b. Cs, Rb
- c. Other nuclides

Note: A DF of 1 is assumed by the BWR-GALE Code for tritium. Noble gases and water activation products are not considered in the liquid code.

2. The system DF for each inlet stream is the product of the individual equipment DFs in each of the subsystems.
3. Equipment that is used optionally (as required) and not included in the normal flow scheme should not be considered in calculating the overall system DF.

Table 1-3 shows the decontamination factors to be used for BWR systems.

The following example illustrates the calculation of the decontamination factor for a low-purity waste treatment system: Assume that low-purity wastes are collected; processed through a filter, an evaporator, and a mixed-bed polishing demineralizer; and collected for sampling. If required to meet discharge criteria, the contents of the waste sample (test) tank are processed through a mixed-bed demineralizer for additional radionuclide removal. This example may be summarized graphically as:



Extracting from Table 1-3 gives the following values for the example:

	Filter	Evaporator	Demineralizer 1	Demineralizer 2	Product
Halogens	1	10^3	10	1	10^4
Cs, Rb	1	10^4	10	1	10^5
Other Nuclides	1	10^4	10	1	10^5

These values were obtained as follows:

- A DF of 1.0 was applied to all nuclides for the filter.
- A DF of 10^3 for halogens and 10^4 for Cs, Rb, and other nuclides was applied for the radwaste evaporator.
- A DF of 10 was applied for halogens, Cs, Rb, and other nuclides and for the evaporator condensate polishing demineralizer.
- A DF of 1 was applied to the second demineralizer since this demineralizer's use is optional and it is not used for normal operations.
- The product of the DFs was obtained by combining the first four columns for each radionuclide.

TABLE 1-3
DECONTAMINATION FACTORS FOR BWR LIQUID WASTE TREATMENT SYSTEMS

TREATMENT SYSTEM	DECONTAMINATION FACTOR		
	Anion	Cs, Rb	Other Nuclides
Demineralizers			
Mixed-bed reactor coolant cleanup	10	2	10
Condensate (deep bed)	10	2	10
High-purity waste	$10^2(10)^*$	10(10)	$10^2(10)$
Low-Purity Waste			
Mixed bed	$10^2(10)$	2(10)	$10^2(10)$
Cation bed	1(1)	10(10)	$10^2(10)$
Anion bed	$10^2(10)$	1(1)	1(1)
Powdex (any system)	10(10)	2(10)	10(10)
Evaporators	All Nuclides Except Iodine		Iodine
Miscellaneous	10^4		10^3
Detergent wastes	10^2		10^2
Reverse Osmosis	All Nuclides		
Laundry wastes	30		
Other liquid wastes	10		
Filters	DF of 1.0 for all nuclides		

* For an evaporator polishing demineralizer or for the second demineralizer in series, the DF is given in parentheses.

Thus in Card 10 the following would be entered: in spaces 21-28, "10,000"; in spaces 34-41, "100,000"; and in spaces 47-54, "100,000."

1.5.2.9.3 Collection Time for Liquid Wastes (Cards 11, 14, 17, 20 -- Spaces 29-33)

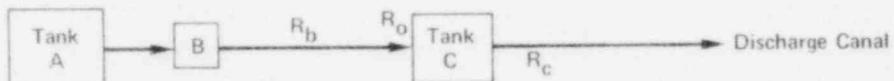
Collection time prior to processing is based on the input flow calculated above. Where redundant tanks are provided, assume the collection tank to be filled to 80% capacity. If only one tank is provided, assume the tank to be filled to 40% capacity. For example, if flow from a 1,000-gal/day floor drain is collected in two 20,000-gallon tanks prior to processing, collection time would be calculated as follows:

$$\text{Collection time } (T_c) = \frac{(20,000 \text{ gal})(0.8)}{1,000 \text{ gal/day}} = 16 \text{ days}$$

Then, for this example, "16" should be entered in spaces 29-33 on Card 14.

1.5.2.9.4 Processing and Discharge Time (Cards 11, 14, 17, 20 -- Spaces 48-53)

Decay during processing and discharge of liquid wastes is shown graphically as follows:



where

- A is the capacity of the initial tank in the flow scheme, in gal;
- B is the limiting process based on equipment flow capacity, dimensionless;
- C is the capacity of the final tank in the flow scheme prior to discharge, in gal;
- R_b is the equipment flow capacity of process B, in gal/day;
- R_c is the flow capacity of the Tank C discharge pump, in gal/day; and
- R_o is the rate of flow of additional wastes inputs to Tank C, in gal/day.

T_p , the process time credited for decay, is calculated as follows, in days:

$$T_p = \frac{0.8A}{R_b}$$

T_d , the discharge time -- 50% credited for decay, is calculated as follows, in days:

$$T_d = \frac{0.8C}{R_c}$$

After performing the above two calculations, calculate whether credit may be taken for decay during processing by determining whether

$$0.8C > T_p R_b + R_o$$

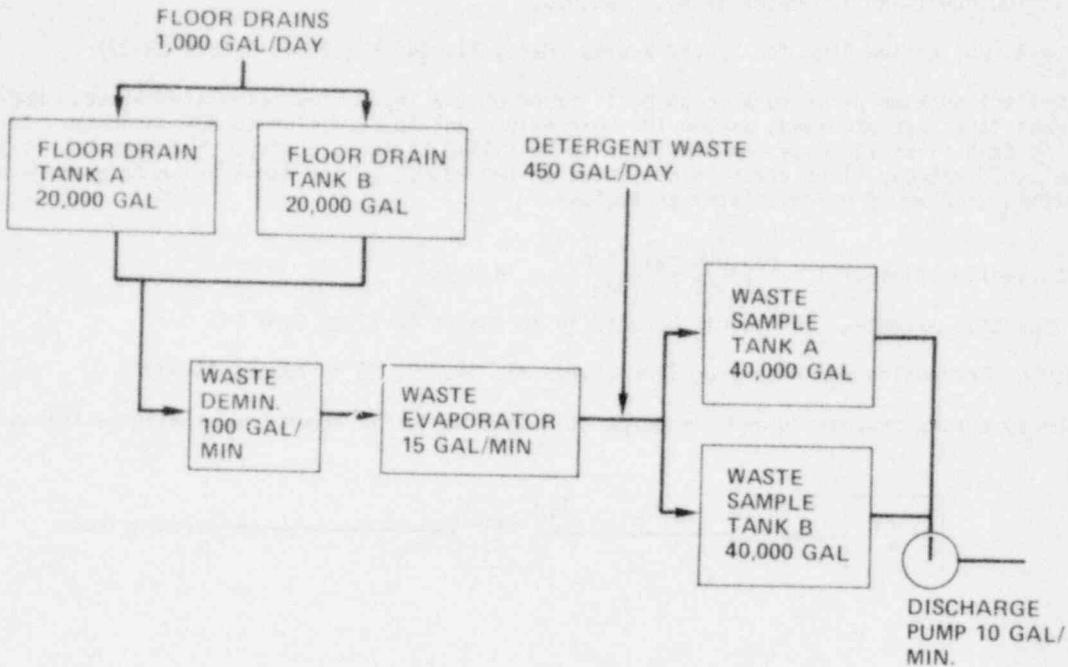
If so, then

$$\text{Decay} = T_p + 0.5T_d$$

where "Decay" is the new processing and discharge time to be entered in spaces 48-53 of the third card for each input stream (Cards 11, 14, 17, and 20).

If, however, $0.8 \leq T_p(R_b + R_o)$, T_p is used for the holdup time during processing, since Tank C may be discharged before Tank A has been completely processed. In this case, the T_p value should be entered in spaces 48-53 of the third card.

For example, for the following input waste stream:



Decay time during processing and discharge would be calculated as follows:

$$\text{Process Time } (T_p) = \frac{(0.8)(20,000 \text{ gal})}{(15 \text{ gal/min})(1440 \text{ min/day})} = 0.7 \text{ day}$$

$$\text{Discharge Time } (T_d) = \frac{(0.8)(40,000 \text{ gal})}{(10 \text{ gal/min})(1440 \text{ min/day})} = 3 \text{ days}$$

Then, checking for decay credit, $0.8C/(R_b + R_0) = 1.45$ days, which is greater than T_p ; therefore, credit is taken for $(T_p + 0.5T_d)$ or 2.2 days for processing and discharge. The input on spaces 48-53 to the Code is 2.2 days for processing and discharge time.

1.5.2.9.5 Fraction of Wastes Discharged (Cards 11, 14, 17, and 20 -- Spaces 72-77)

The percent of the wastes discharged after processing may vary between 1% and 100% based on the capability of the system to process liquid waste during equipment downtime, waste volume surges, tritium control requirements, and tank surge capacity. A minimum value of 1% discharge for high-purity wastes and 10% discharge for other wastes is used when the radwaste system is designed for maximum waste recycle, the system capacity is sufficient to process wastes for reuse during equipment downtime and anticipated operational occurrences, and a discharge route is provided.

The BWR-GALE Code calculates the release of radioactive materials in liquid waste from the four inlet streams after processing. Releases included in each stream are:

1. High-Purity Waste - Combined releases from equipment drains and sumps.
2. Low-Purity Waste - Combined releases from floor drains and sumps.
3. Chemical Waste - Combined releases from laboratory and decontamination wastes and from demineralizer regenerant solutions according to the design of the condensate demineralizer system. If a filter/demineralizer (Powdex) system is used, the laboratory and decontamination wastes are combined with the low-purity waste or solidified in the solid waste system.
4. Detergent Waste System - Combined releases from laundry operations, equipment decontamination solutions, and personnel decontamination showers.

1.5.2.10 Card 21: Gland Seal Steam Flow

Enter in spaces 73-80 of Card 21 the steam flow (in 10^3 lb/hr) to the turbine gland seal, as follows:

1. If main steam is used for the sealing steam, enter a flow rate 0.001 times the main steam flow entered previously on Card 3.
2. If clean (nonradioactive) steam from an auxiliary boiler is used for sealing steam, enter a zero in spaces 73-80.

1.5.2.11 Card 22: Mass of Steam in Reactor Vessel (SAR/ER)

Enter in spaces 73-80 the mass of steam in the reactor vessel (in 10^6 lb).

1.5.2.12 Card 23: Gland Seal Holdup Time (SAR/ER)

Enter in spaces 73-80 the design holdup (in hr) for gases vented from the gland seal condenser.

1.5.2.13 Card 24: Holdup Time for Condenser Air Ejector Offgas (SAR/ER)

Enter in spaces 73-80 the design holdup time (in hr) for offgases from the main condenser air ejector to be processed through the offgas treatment system, e.g., a 10-minute holdup time prior to cryogenic distillation.

1.5.2.14 Card 25: Containment Building Releases

1. If ventilation exhaust air is treated through charcoal adsorbers, enter YES in spaces 43-45. If no treatment is provided, leave spaces 43-45 blank.
2. If ventilation exhaust air is treated through HEPA filters, enter YES in spaces 52-54. If no treatment is provided, leave spaces 52-54 blank.

1.5.2.15 Card 26: Turbine Building Releases

1. If ventilation exhaust air is treated through charcoal adsorbers, enter YES in spaces 43-45. If no treatment is provided, leave spaces 43-45 blank.

2. If ventilation exhaust air is treated through HEPA filters, enter YES in spaces 52-54. If no treatment is provided, leave these spaces blank.

3. If "clean steam" or other acceptable special design features are provided on valves 2-1/2 inches and larger to reduce steam leakage, enter YES in spaces 68-70. If the above features are not provided, leave spaces 68-70 blank.

1.5.2.16 Card 27: Fraction of Iodine Released from Turbine Gland Seal Condenser Vent

1. Enter 1.0 in spaces 73-80 if the noncondensables are released from the turbine gland seal condenser without treatment or if clean steam is used.
2. Enter 0.1 in spaces 73-80 if, prior to release, the noncondensables are processed through charcoal adsorbers having a 90% efficiency.

1.5.2.17 Card 28: Fraction of Iodine Released from the Condenser Air Ejector Offgas Treatment System

1. Enter 1.0 in spaces 73-80 if the offgas is released without treatment.
2. Enter 0.1 in spaces 73-80 if, prior to release, the offgas is processed through a charcoal adsorber having a 90% efficiency.
3. Enter a zero in spaces 73-80 if the offgas is processed through a charcoal delay system.
4. Enter 1.0 in spaces 73-80 if the offgas is processed through a cryogenic distillation system (removal of iodine by the cryogenic distillation system is built into the Code - see Card 30).

1.5.2.18 Card 29: Auxiliary Building Releases

1. If ventilation exhaust air is treated through charcoal adsorbers, enter YES in spaces 43-45. If no treatment is provided, leave blank.

2. If ventilation effluent is treated through HEPA filters, enter YES in spaces 52-54. If no treatment is provided, leave blank.

1.5.2.19 Card 30: Radwaste Building Releases

1. If ventilation exhaust air is treated through charcoal adsorbers, enter YES in spaces 43-45. If no treatment is provided, leave blank.
2. If ventilation exhaust air is treated through HEPA filters, enter YES in spaces 52-54. If no treatment is provided, leave blank.

1.5.2.20 Card 31: Condenser Air Ejector Offgas Treatment System (SAR/ER)

1. Enter 1 in space 80 if charcoal delay system is used to treat the offgas from the condenser air ejector.
2. Enter 2 in space 80 if the offgas from the condenser air ejector is processed by the cryogenic distillation.
3. Enter a zero in space 80 if the offgas is not treated either through a charcoal delay system or by cryogenic distillation.

Note: Cards 31, 32, 33, and 34 are left blank if a charcoal delay system is not used to treat the offgases from the condenser air ejector. The blank cards are included in the card deck.

1.5.2.21 Card 32: Dynamic Adsorption Coefficient for Krypton

Enter in spaces 73-80 the dynamic adsorption coefficient for Kr based on the system design and the dynamic adsorption coefficients noted below.

DYNAMIC ADSORPTION COEFFICIENT (cm ³ /g)		
	OPERATING 77°F DEW POINT 45°F	OPERATING 77°F DEW POINT 0°F
Kr	18.5	25
OPERATING 0°F DEW POINT -20°F		105

1.5.2.22 Card 33: Dynamic Adsorption Coefficient for Xenon

Enter in spaces 73-80 the dynamic adsorption coefficient for Xe based on the system design and dynamic adsorption coefficients noted below.

DYNAMIC ADSORPTION COEFFICIENT (cm ³ /g)		
	OPERATING 77°F DEW POINT 45°F	OPERATING 77°F DEW POINT 0°F
Xe	330	440
OPERATING 0°F DEW POINT -20°F		2410

1.5.2.23 Card 34: Number of Main Condenser Shells (SAR/ER)

Enter in spaces 73-80 the number of shells in the main condenser.

1.5.2.24 Card 35: Mass of Charcoal in Charcoal Delay System (SAR/ER)

Enter in spaces 73-80 the mass of charcoal (in 10³ lb) used in the charcoal delay system.

1.5.2.25 Card 36: Detergent Waste

1. If the plant does not have an onsite laundry, enter a zero in spaces 73-80.
2. If the plant has an onsite laundry and detergent wastes are released without treatment, enter 1.0 in spaces 73-80.
3. If detergent wastes are treated prior to discharge, enter the fraction of radionuclides remaining after treatment (1/DF) in spaces 73-80. The parameters in Chapter 2 are used in determining the DF for the treatment applied to detergent waste.

CHAPTER 2. PRINCIPAL PARAMETERS USED IN BWR SOURCE TERM CALCULATIONS AND THEIR BASES

2.1 INTRODUCTION

The principal parameters used in source term calculations have been compiled to standardize the calculation of radioactive source terms. The source term is defined as the calculated average quantity of radioactive material released annually to the environment from a nuclear power reactor during normal operation, including anticipated operational occurrences. The parameters used in the calculations are the average values expected over the life of the plant. Normal operation includes anticipated operational occurrences that deviate from steady-state operation.

The following sections describe parameters used in the evaluation of radwaste treatment systems. The parameters have been derived from reactor operating experience where data were available. Where operating data were inconclusive or not available, information was drawn from laboratory and field tests and from engineering judgment. The bases for the source term parameters explain the reasons for choosing the numerical values listed. A list of references used in developing the parameters is also included.

The parameters in the BWR-GALE Code are updated as additional operating data become available. The source term parameters used are believed to provide a realistic assessment of reactor and radwaste system operation.

2.2 PRINCIPAL PARAMETERS AND THEIR BASES

2.2.1 THERMAL POWER LEVEL

2.2.1.1 Parameter

The maximum thermal power level (MWh) evaluated for safety considerations in the Safety Analysis Report.

2.2.1.2 Bases

The power level used in the source term BWR-GALE Code is the maximum power level evaluated for safety considerations in the Safety Analysis Report. Using this value, the evaluation of the radwaste management systems need not be repeated when the applicant applies for a stretch power license at a later date. Past experience indicates that most utilities request approval to operate at maximum power soon after reaching commercial operation.

2.2.2 PLANT CAPACITY FACTOR

2.2.2.1 Parameter

Plant capacity factor of 80%, i.e., 292 effective full power days.

2.2.2.2 Bases

The source term calculations are based on a plant capacity factor of 80% averaged over the 30-year operating life of the plant, i.e., the plant operates at 100% power 80% of the time. The plant capacity factors experienced at BWRs are listed in Table 2-1 for the period 1961 through 1974.

The average plant capacity factors listed indicate that the 80% factor assumed is higher than the average factors experienced. However, it is expected that the maintenance and refueling problems that have contributed to the low capacity factors will be overcome.

2.2.3 RADIONUCLIDE CONCENTRATIONS IN THE REACTOR COOLANT

2.2.3.1 Parameter

Table 2-2 lists the expected radionuclide concentrations in the reactor coolant and steam for BWRs with design parameters within the ranges listed in Table 2-3. Should any design parameter be outside the ranges in Table 2-3, adjust the concentrations in Table 2-2, using Tables 2-4 and 2-5. Figure 2-1 shows the graphical relationship of the design parameters.

TABLE 2-1
PLANT CAPACITY FACTORS AT OPERATING BWRs*
(in %)

<u>FACILITY</u>	<u>INITIAL CRITICALITY</u>	1968	1969	1970	1971	1972	1973	1974
Dresden 1	10/15/59	52	48	78	35	61	40	21
Big Rock Point	9/27/62	68	64	58	59	57	67	54
Humboldt Bay	2/16/63	82	68	76	61	59	70	61
Oyster Creek	5/3/69			74	78	77	64	66
Nine Mile Point 1	9/5/69				63	62	68	63
Dresden 2	1/7/70				39	47	74	51
Millstone 1	10/26/70				63	55	34	63
Monticello	12/10/70					74	68	57
Dresden 3	1/31/71					67	54	47
Quad Cities 1	10/18/71						70	51
Vermont Yankee	3/24/72						44	59
Quad Cities 2	4/26/72						74	68
Pilgrim 1	6/16/72						72	34
Average		67	60	72	57	62	61	53

* From "U.S. Nuclear Power Reactors," Atomic Energy Commission, WASH-1203-68 to 73, Table 1, "Selected Operating Statistics." Plant capacity factors listed are for the calendar year(s) following a period of at least six months since initial criticality. Operating BWRs not included in the table are Browns Ferry 1 and Peach Bottom 2, which achieved criticality during CY-1973. The LaCrosse Nuclear Power Station was not included since it is not considered to be representative of current power reactors.

TABLE 2-2
RADIONUCLIDE CONCENTRATIONS
IN BOILING WATER REACTOR COOLANT AND MAIN STEAM*
(in $\mu\text{Ci/g}$)

<u>ISOTOPE</u>	<u>REACTOR WATER</u>	<u>REACTOR STEAM</u>
<u>Noble Gases</u>		
Kr-83m		1.1(-3)**
Kr-85m		1.9(-3)
Kr-85		6.0(-6)
Kr-87		6.6(-3)
Kr-88		6.6(-3)
Kr-89		4.1(-2)
Kr-90		9.0(-2)
Kr-91		1.1(-1)
Kr-92		1.1(-1)
Kr-93		2.9(-2)
Kr-94		7.2(-3)
Kr-95		6.6(-4)
Kr-97		4.4(-6)
Xe-131m		4.7(-6)
Xe-133m		9.0(-5)
Xe-133		2.6(-3)
Xe-135m		8.4(-3)
Xe-135		7.2(-3)
Xe-137		4.7(-2)
Xe-138		2.8(-2)
Xe-139		9.0(-2)
Xe-140		9.6(-2)
Xe-141		7.8(-2)
Xe-142		2.3(-2)
Xe-143		3.8(-3)
Xe-144		1.8(-4)
<u>Halogens</u>		
Br-83	3(-3)	6(-5)
Br-84	5(-3)	1(-4)
Br-85	3(-3)	6(-5)
I-131	5(-3)	1(-4)
I-132	3(-2)	6(-4)
I-133	2(-2)	4(-4)
I-134	5(-2)	1(-3)
I-135	2(-2)	4(-4)
<u>Cesium and Rubidium</u>		
Rb-89	5(-3)	5(-6)
Cs-134	3(-5)	3(-8)
Cs-136	2(-5)	2(-8)
Cs-137	7(-5)	7(-8)
Cs-138	1(-2)	1(-5)

*The reactor water concentration is specified at the nozzle where reactor water leaves the reactor vessel. Similarly, the reactor steam concentration is specified at time 0.

** $1.1(-3) = 1.1 \times 10^{-3}$.

TABLE 2-2 (Continued)

ISOTOPE	REACTOR WATER	REACTOR STEAM
<u>Water Activation Products</u>		
N-13	5(-2)	7(-3)
N-16	6(+1)	5(+1)
N-17	9(-3)	2(-2)
O-19	7(-1)	2(-1)
F-18	4(-3)	4(-3)
<u>Tritium*</u>		
H-3	1(-2)	1(-2)
<u>Other Nuclides</u>		
Na-24	9(-3)	9(-6)
P-32	2(-4)	2(-7)
Cr-51	5(-3)	5(-6)
Mn-54	6(-5)	6(-8)
Mn-56	5(-2)	5(-5)
Fe-55	1(-3)	1(-6)
Fe-59	3(-5)	3(-8)
Co-58	2(-4)	2(-7)
Co-60	4(-4)	4(-7)
Ni-63	1(-6)	1(-9)
Ni-65	3(-4)	3(-7)
Cu-64	3(-2)	3(-5)
Zn-65	2(-4)	2(-7)
Zn-69	2(-3)	2(-6)
Sr-89	1(-4)	1(-7)
Sr-90	6(-6)	6(-9)
Sr-91	4(-3)	4(-6)
Sr-92	1(-2)	1(-5)
Y-91	4(-5)	4(-8)
Y-92	6(-3)	6(-6)
Y-93	4(-3)	4(-6)
Zr-95	7(-6)	7(-9)
Zr-97	5(-6)	5(-9)
Nb-95	7(-6)	7(-9)
Nb-98	4(-3)	4(-6)
Mo-99	2(-3)	2(-6)
Tc-99m	2(-2)	2(-5)
Tc-101	9(-2)	9(-5)
Tc-104	8(-2)	8(-5)
Ru-103	2(-5)	2(-8)
Ru-105	2(-3)	2(-6)
Ru-106	3(-6)	3(-9)
Ag-110m	1(-6)	1(-9)
Te-129m	4(-5)	4(-8)
Te-131m	1(-4)	1(-7)

* Measured values increased to account for liquid recycle.

TABLE 2-2 (Continued)

<u>ISOTOPES</u>	<u>REACTOR WATER</u>	<u>REACTOR STEAM</u>
Te-132	1(-5)	1(-8)
Ba-139	1(-2)	1(-5)
Ba-140	4(-4)	4(-7)
Ba-141	1(-2)	1(-5)
Ba-142	6(-3)	6(-6)
La-142	5(-3)	5(-6)
Ce-141	3(-5)	3(-8)
Ce-143	3(-5)	3(-8)
Ce-144	3(-6)	3(-9)
Pr-143	4(-5)	4(-8)
Nd-147	3(-6)	3(-9)
W-187	3(-4)	3(-7)
Np-239	7(-3)	7(-6)

TABLE 2-3
PARAMETERS USED TO DESCRIBE THE REFERENCE BOILING WATER REACTOR

<u>PARAMETER</u>	<u>SYMBOL</u>	<u>UNITS</u>	<u>NOMINAL VALUE</u>	<u>RANGE</u>	
				<u>MAXIMUM</u>	<u>MINIMUM</u>
Thermal power	P	Mwt	3400	3800	3000
Weight of water in the reactor vessel	WP	lb	3.8(5)*	4.2(5)	3.4(5)
Cleanup demineralizer flow rate	FA	lb/hr	1.3(5)	1.5(5)	1.1(5)
Steam flow rate	FS	lb/hr	1.5(7)	1.7(7)	1.3(7)
Ratio of condensate demineralizer flow rate to steam flow rate	NC	-	1.0	1.0	0.8

* $3.8(5) = 3.8 \times 10^5$

TABLE 2-4
VALUES USED IN DETERMINING ADJUSTMENT FACTORS FOR
BOILING WATER REACTORS

SYMBOL	DESCRIPTION	NOBLE GASES	HALOGENS	Cs, Rb	WATER ACTIVATION PRODUCTS	TRITIUM	OTHER NUCLIDES
NA	Fraction of material removed in the reactor water cleanup system	0.0	0.9	0.5	0.0	0.0	0.9*
NB	Fraction of material removed by the condensate demineralizers	0.0	0.9	0.5	0.0	0.0	0.9*
NS	Ratio of concentration in reactor steam to the concentration in reactor water	**	0.02	0.001	***	1.0	0.001
R	Removal rate from the reactor water (hr^{-1})†	**	1.0	0.19	***	++	0.34

* These represent effective removal terms and include other mechanisms such as plateout. Plateout would be applicable to nuclides such as Mo and corrosion products.

** All noble gases released from the core are transported rapidly out of the reactor water to the reactor steam and are stripped from the system in the main condenser. Therefore the concentration in the reactor water is negligible and the steam concentration is approximately equivalent to the ratio of the release rate and the steam flow rate.

*** Water activation products exhibit varying chemical and physical properties in reactor coolant which are not well defined. However, most are stripped off as gases. They are not effectively removed by the demineralizers of the systems, but their concentrations are controlled by decay.

† These values of R apply to the reference BWR whose parameters are given in Table 2-3 and have been used in developing Table 2-5. For BWRs not included in Table 2-3, the appropriate value for R may be determined by the following equation:

$$R = \frac{FA \cdot NA + NC \cdot FS \cdot NS \cdot NB}{WP} \text{ for halogens, Cs, Rb, and other nuclides}$$

where the symbols are defined in this table and Table 2-3. The values for R for noble gases and water activation products are not used in the adjustment factors of Table 2-5.

++ The tritium concentrations in the reactor water and the steam are expected to be equal. They are controlled by loss of water from the main coolant system by evaporation or leakage. The concentration is therefore given by the ratio of the appearance rate in the coolant, which is about 100 Ci/yr, and the total loss from the system.

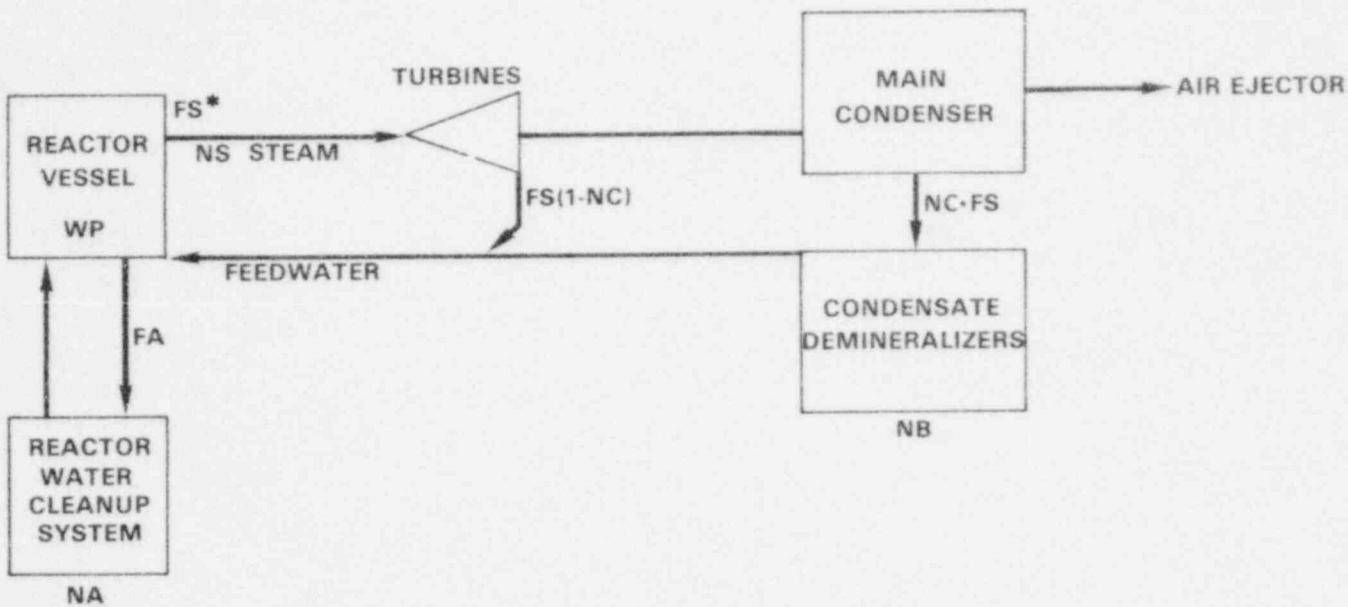
TABLE 2-5
ADJUSTMENT FACTORS FOR BOILING WATER REACTORS

<u>NUCLIDES</u>	<u>REACTOR WATER</u>	<u>REACTOR STEAM</u>
Noble gases*	1.0	1.0
Halogens**	$\frac{P}{WP} (110 \frac{lb}{Mwt}) \frac{1.0 + \lambda}{R + \lambda}$	$\frac{P}{WP} (110 \frac{lb}{Mwt}) \frac{1.0 + \lambda}{R + \lambda}$
Cs, Rb	$\frac{P}{WP} (110 \frac{lb}{Mwt}) \frac{0.19 + \lambda}{R + \lambda}$	$\frac{P}{WP} (110 \frac{lb}{Mwt}) \frac{0.19 + \lambda}{R + \lambda}$
Water activation products	1.0	1.0
Tritium***	1.0	1.0
Other nuclides	$\frac{P}{WP} (110 \frac{lb}{Mwt}) \frac{0.34 + \lambda}{R + \lambda}$	$\frac{P}{WP} (110 \frac{lb}{Mwt}) \frac{0.34 + \lambda}{R + \lambda}$

*Assumes that the ratio of power to steam flow is essentially the same for all BWRs.

** λ is the isotope's decay constant (hr^{-1}).

***The tritium concentrations in the reactor water and the steam are expected to be equal. They are controlled by loss of water from the main coolant system by evaporation or leakage. The concentration is therefore given by the ratio of the appearance rate in the coolant, which is about 100 Ci/yr, and the total loss from the system.



* SYMBOLS ARE DEFINED IN TABLES 2-3 AND 2-4

FIGURE 2-1
REMOVAL PATHS FOR THE REFERENCE
BOILING WATER REACTOR

2.2.3.2 Bases

The radionuclide concentrations, adjustment factors, and procedures for effecting adjustments are based on the values and methods proposed by the ANS 18.1 Working Group draft standard for boiling water reactor source terms (Ref. i). The values in Table 2-2 provide a set of typical radionuclide concentrations in the reactor coolant and steam for reactor designs within the parameters specified in Table 2-3. The values in Table 2-2 were those judged by the ANS Working Group to be representative of radionuclide concentrations in a BWR over its lifetime based on the currently available data and models (Refs. 2 and 3). It is recognized that some systems will have design parameters that are outside the ranges specified in Table 2-3. For that reason a means of adjusting the concentrations to the actual design parameters has been provided in Tables 2-4 and 2-5. The adjustment factors in Tables 2-4 and 2-5 are based on the following expression:

$$C = \frac{S}{W(\lambda + R)k}$$

where

- C is the specific activity, in $\mu\text{Ci/g}$;
- k is a conversion factor, 454 g/lb;
- R is the removal rate of the isotope from the system due to demineralization, leakage, etc., in hr^{-1} ;
- s is the rate of release to and/or production of the isotope in the system, in $\mu\text{Ci/hr}$;
- w is the fluid weight, in lb; and
- λ is the decay constant, in hr^{-1} .

The following sample calculations illustrate the method by which the BWR-GALE Code will adjust the radionuclide concentrations in Table 2-2. As indicated in Table 2-5, adjustment factors will be calculated only for halogens, Cs, Rb, and other nuclides.

As an example, the Barton Nuclear Station parameters compare with the range values in Table 2-3 as follows:

Parameter	Barton Station Value	Range Values
Thermal power level (Mwt)	3758	3000-3800
Water weight in vessel (lb)	4.9×10^5	$3.4 \times 10^5 - 4.2 \times 10^5$
Cleanup demineralizer flow (lb/hr)	1.5×10^5	$1.1 \times 10^5 - 1.5 \times 10^5$
Steam flow rate (lb/hr)	15.4×10^6	$13.0 \times 10^6 - 17.0 \times 10^6$
Condensate demineralizer flow fraction	0.75	0.8 - 1.0

Since in this example two of the parameters (water weight in vessel and condensate demineralizer flow fraction) are outside the range, adjusted values of the three types of radionuclide concentrations are calculated using the actual value of each parameter, as follows:

1. Halogens (I-131 is used as an example) -- Using the equation for halogens in Table 2-5, the adjustment factor A is calculated as follows:

$$A = \frac{P}{WP} (110) \frac{1.0 + \lambda}{R + \lambda} \quad (2-1)$$

where the terms in the equation are as defined in Tables 2-3 and 2-4.

In calculating A, the variable R is calculated first, using the equation given in Table 2-4:

$$R = \frac{FA \cdot NA + NC \cdot FS \cdot NS \cdot NB}{WP} \quad (2-2)$$

where the terms in the equation are as defined in Tables 2-3 and 2-4.

Using the Barton Station parameters given above and the halogen parameters given in Table 2-4 and substituting in Equation (2-1) gives

$$R = \frac{1.5 \times 10^5 \times 0.9 + 0.75 \times 15.4 \times 10^6 \times 0.02 \times 0.9}{4.9 \times 10^5} = 0.7$$

Then, using this value of R in Equation (2-1):

$$A = \frac{3758}{4.9 \times 10^5} (110) \frac{1.0 + 3.6 \times 10^{-3}}{0.7 + 3.6 \times 10^{-3}} = 1.2$$

The adjusted I-131 concentration

$$\begin{aligned} &= (\text{adjustment factor}) \times (\text{standard I-131 concentration}) \\ &= 1.2 \times 5 \times 10^{-3} \mu\text{Ci/g} = 6.0 \times 10^{-3} \mu\text{Ci/g} \end{aligned}$$

2. Cs, Rb (Cs-137 is used as an example) -- Using the equation for Cs and Rb in Table 2-5, the adjustment factor A is calculated as follows:

$$A = \frac{P}{WP} (110) \frac{0.19 + \lambda}{R + \lambda} \quad (2-3)$$

where the terms in the equation are as defined in Tables 2-3 and 2-4.

In calculating A, the variable R is calculated first, using Equation (2-2). The Cs and Rb parameters given in Table 2-4 and the Barton Station parameters are used in the equation.

$$R = \frac{1.5 \times 10^5 \times 0.5 + 0.75 \times 15.4 \times 10^6 \times 0.001 \times 0.5}{4.9 \times 10^5} = 0.17$$

Then, using this value of R in Equation (2-3) above:

$$A = \left(\frac{3758}{4.9 \times 10^5} \right) (110) \frac{(0.19 + 2.6 \times 10^{-6})}{(0.17 + 2.6 \times 10^{-6})} = 0.97$$

The adjusted Cs-137 concentration

$$\begin{aligned} &= (\text{adjustment factor}) \times (\text{standard Cs-137 concentration}) \\ &= 0.97 \times 7 \times 10^{-5} \mu\text{Ci/g} = 6.8 \times 10^{-5} \mu\text{Ci/g} \end{aligned}$$

3. Other Nuclides (Na-24 is used as an example) -- Using the equation for other nuclides in Table 2-5, the adjustment factor A is calculated as follows:

$$A = \frac{P}{WP} (110) \frac{0.34 + \lambda}{R + \lambda} \quad (2-4)$$

where the terms in the equation are as defined in Tables 2-3 and 2-4.

In calculating A, the variable R is calculated first, using Equation (2-2). The other nuclide parameters given in Table 2-4 and the Barton Station parameters are used in the equation:

$$R = \frac{1.5 \times 10^5 \times 0.9 + 0.75 \times 15.4 \times 10^6 \times 0.001 \times 0.9}{4.9 \times 10^5} = 0.3$$

Then, using this value of R in Equation (2-4):

$$A = \left(\frac{3758}{4.9 \times 10^5} \right) (110) \left(\frac{0.34 + 4.62 \times 10^{-2}}{0.3 + 4.62 \times 10^{-2}} \right) = 0.95$$

The adjusted concentration of Na-24

$$\begin{aligned} &= (\text{adjustment factor}) \times (\text{standard Na-24 concentration}) \\ &= 0.95 \times 9 \times 10^{-3} \mu\text{Ci/g} = 8.6 \times 10^{-3} \mu\text{Ci/g} \end{aligned}$$

The noble gas concentrations in Table 2-2 are based on an offgas release rate of 60,000 $\mu\text{Ci/sec}$ measured at a 30-minute decay. A summary of noble gas release rates from a number of operating BWRs in 1971-72 is given in Table 2-6 and a similar summary for 1973-74 is given in Table 2-7. The data in these tables are limited to measurements from BWRs larger than 1000 MWT with more than one year of operating experience. The average of the noble gas release rates in Tables 2-6 and 2-7, based on the effective full power days of operation and normalized to 3400 MWT, is 60,000 $\mu\text{Ci/sec}$.

A carryover factor of 0.02 is used to calculate the halogen concentrations in the main steam in Table 2-2. This carryover factor is derived from data taken at operating reactors (Refs. 2, 3, 4, and 5) which are listed in Table 2-8. The average of the data in Table 2-8 is 0.018 for halogen (iodine) carryover.

The category "Other nuclides" includes Mo, Y, and Tc which are generally present in colloidal suspensions or as "crud." Although the actual removal mechanism for Y, Mo, and Tc is expected to be plateout or filtration, the quantitative effect of renewal is expected to be commensurate with the removal of ionic impurities by ion exchange (within the accuracy of the calculations) and consequently plateout of these nuclides is included in the parameters for ion exchange.

2.2.4 GASEOUS RELEASES FROM BUILDING VENTILATION SYSTEMS

2.2.4.1 Parameter

The noble gas, iodine, and radioactive particulate releases from ventilation systems for facilities with the BWR/6, Mark III containment design, prior to treatment, are shown in Table 2-9.

2.2.4.2 Bases

The iodine-131 releases from building ventilation effluents are based on measurements made at operating reactors. The measurements were made during normal operation and during plant shutdowns. The data are given in Tables 2-10 through 2-15. These data show that the release rates during plant shutdown differ from the release rates during plant operation. The ratio of releases during shutdowns to releases during normal operations, assuming a plant capacity factor of 80%, is used to calculate annual releases that consider both normal operation and shutdown releases.

Table 2-13 gives the iodine-131 release rates during normal operation and during plant shutdowns for the Oyster Creek turbine building as 0.024 $\mu\text{Ci/sec}$ and 0.081 $\mu\text{Ci/sec}$, respectively. Using an 80% plant capacity factor, the ratio of releases due to normal operation and shutdowns to the releases during normal operation only can be expressed as

$$\frac{(0.024 \mu\text{Ci/sec})(0.8)}{(0.024 \mu\text{Ci/sec})(0.8)} + \frac{(0.081 \mu\text{Ci/sec})(0.2)}{(0.024 \mu\text{Ci/sec})(0.8)} = 1.8$$

Similarly, from Table 2-13 the ratio of releases due to normal operation and shutdowns to the releases during normal operation for Vermont Yankee is 1.7. Using the average of these ratios, the average annual turbine building releases during normal operation from Table 2-12 are normalized to obtain a total annual release as indicated below:

$$\frac{(1.8 + 1.7)}{2} (0.11 \text{ Ci/yr}) = 0.19 \text{ Ci/yr total I-131 released}$$

TABLE 2-6
SUMMARY OF NOBLE GAS RELEASE RATES FOR
OPERATING BWRs (1971-1972)

REACTOR*	NOMINAL POWER (Mwt)	HOLDUP TIME (min)	1971 RELEASES				1972 RELEASES			
			EFPD** (days)	NOBLE GAS (Ci/yr)	AVERAGE (μ Ci/sec)	AVERAGE AT 3400 Mwt (μ Ci/sec)	EFPD** (days)	NOBLE GAS (Ci/yr)	AVERAGE (μ Ci/sec)	AVERAGE AT 3400 Mwt (μ Ci/sec)
Oyster Creek	1930	90	260	516,000	23,000	69,000	280	866,000	36,000	120,000
Nine Mile Point	1850	60	210	253,000	14,000	36,000	230	517,000	27,000	73,000
Millstone 1	2011	50	230	276,000	14,000	30,000	200	721,000	42,000	88,000
Dresden 2, 3***	5052	60	---	---	---	---	420	431,000	35,000	35,000
Monticello	1670	60	---	---	---	---	270	565,000	25,000	76,000
Yearly Average					45,000					71,000

* Reactors smaller than 1000 Mwt (Big Rock Point, Dresden 1, Humboldt Bay, Lacrosse) are not included. Quad Cities 1 and 2, Vermont Yankee, and Pilgrim 1 were undergoing startup when this table was compiled and are not included.

** Effective full power days of operation.

*** Dresden 2 and 3 are considered as two reactors.

TABLE 2-7
SUMMARY OF NOBLE GAS RELEASE RATES FOR
OPERATING BWRs (1973-1974)

REACTOR *	NOMINAL POWER (Mwt)	HOLDUP TIME (min)	1973 RELEASES				1974 RELEASES			
			EFPD ** (days)	NOBLE GAS (Ci/yr)	AVERAGE ($\mu\text{Ci/sec}$)	AVERAGE AT 3400 Mwt ($\mu\text{Ci/sec}$)	EFPD ** (days)	NOBLE GAS (Ci/yr)	AVERAGE ($\mu\text{Ci/sec}$)	AVERAGE AT 3400 Mwt ($\mu\text{Ci/sec}$)
Oyster Creek	1930	90	230	812,000	35,000	120,000	240	280,000	14,000	47,000
Nine Mile Point 1	1850	60	250	872,000	40,000	110,000	240	617,000	30,000	75,000
Millstone 1	2011	50	120	69,500	7,000	21,000	230	912,000	46,000	99,000
Dresden 2, 3 ***	5054	60	440	875,000	46,000	43,000	340	628,000	21,000	20,000
Monticello	1670	60	250	732,000	34,000	95,000	220	1,490,000	78,000	220,000
Quad Cities 1, 2 ***	5022	60	510	903,000	41,000	42,000	430	1,049,000	28,000	26,000
Vermont Yankee	1593	60	160	187,000	20,000	63,000	+			
Pilgrim 1	1998	60	270	230,000	10,000	25,000	130	546,000	49,000	126,000
Yearly Average					61,000					73,000

* Reactors smaller than 1000 Mwt (Big Rock Point, Dresden 1, Humboldt Bay, Lacrosse) are not included.
 Reactors undergoing startup (Browns Ferry 1, Cooper 1, Duane Arnold, Peach Bottom 2) are not included.

** Effective full power days of operation.

*** Dresden 2, 3 and Quad Cities 1, 2 are both considered as two reactors.

† Vermont Yankee Nuclear Power Station was not included for CY-1974 because of insufficient data regarding effect of augmented offgas treatment system.

TABLE 2-8
REACTOR VESSEL HALOGEN CARRYOVER FACTORS*
OBSERVED AT OPERATING BWRs

REACTOR	POWER LEVEL** (Mwt)	METHOD***	PARTITION FACTOR	REFERENCE
Oyster Creek	(1930)	Condensate	0.018	3
	(1930)	No cleanup	0.018	3
	1830	Condensate	0.019	2
	1830	Condensate	0.021	2
	1830	No cleanup	0.023	2
	1820	Condensate	0.027	4
	(1930)	Condensate	0.023	4
	(1930)	Condensate	0.025	4
	(1930)	No cleanup	0.025	4
	(1930)	No cleanup	0.025	4
Dresden 2	1830	Condensate	0.022	5
	2210	Condensate	0.016	5
	2210	Condensate	0.017	5
	2400	Condensate	0.019	2
	2400	No cleanup	0.010	2
Dresden 3	2100	Condensate	0.022	2
	2100	No cleanup	0.020	2
Millstone	(2011)	Condensate	0.017	3
	2000	Condensate	0.005	2
Monticello	1670	Condensate	0.003	2
	1670	No cleanup	0.005	2
Nine Mile Point	(1850)	Condensate	0.02	3
	(1850)	No cleanup	0.02	3
Quad Cities 1	(2511)	Condensate	0.012	2
	(2511)	No cleanup	0.013	2
Average			0.018	

*Based on iodine-131.

**When test power level is not known, licensed power level is given in parentheses.

***Condensate method - The calculated partition factors are based on the ratio of the iodine-131 concentration in the condensate to that in the reactor water.

No-cleanup method - The calculated partition factors are based on the change in the concentrations of iodine-131 in the reactor water with the cleanup system isolated compared to the concentration with the cleanup system in service.

TABLE 2-9
GASEOUS RELEASES FROM VENTILATION SYSTEMS
(in Ci/yr per reactor)

<u>NUCLIDE</u>	<u>CONTAINMENT BUILDING</u>	<u>AUXILIARY BUILDING</u>	<u>TURBINE* BUILDING</u>	<u>RADIWASTE BUILDING</u>
Kr-83m	**	**	**	**
Kr-85m	3	3	68	**
Kr-85	**	**	**	**
Kr-87	3	3	190	**
Kr-88	3	3	230	**
Kr-89	**	**	**	**
Xe-131m	**	**	**	**
Xe-133m	**	**	**	**
Xe-133	66	66	280	10
Xe-135m	46	46	650	**
Xe-135	34	34	630	45
Xe-137	**	**	**	**
Xe-138	7	7	1440	**
I-131	0.17	0.17	0.19	0.046
I-133	0.68	0.68	0.76	0.18
Co-60	0.01	0.01	0.002	0.09
Co-58	0.0006	0.0006	0.0006	0.0045
Cr-51	0.0003	0.0003	0.013	0.009
Mn-54	0.003	0.003	0.0006	0.036
Fe-59	0.0004	0.0004	0.0005	0.015
Zn-65	0.002	0.002	0.0002	0.001
Zr-95	0.0004	0.0004	0.0001	0.00005
Sr-89	0.00009	0.00009	0.006	0.0005
Sr-90	0.000005	0.000005	0.00002	0.0003
Sb-124	0.0002	0.0002	0.0003	0.00005
Cs-134	0.004	0.004	0.0003	0.0045
Cs-136	0.0003	0.0003	0.00005	0.00045
Cs-137	0.005	0.005	0.0006	0.009
Ba-140	0.0004	0.0004	0.011	0.0001
Ce-141	0.0001	0.0001	0.0006	0.0026

* Less than 1 Ci/yr per reactor.

** For special design features to control leakage from valves in lines 2-1/2 inches and larger, reduce the turbine building leakage rates by a factor of 5.

TABLE 2-10
ANNUAL IODINE-131 RELEASES FROM REACTOR BUILDING
VENTILATION SYSTEMS, NORMAL OPERATION

FACILITY	RELEASE (Ci/yr)*	REFERENCE
Vermont Yankee	0.12	6
Oyster Creek	0.072	2
Oyster Creek	0.04	7
Monticello	0.17	2
Dresden 2	0.096	2
Dresden 3	0.3	2
Millstone 1	0.03	8
Quad Cities 1	0.096	9
Nine Mile Point 1	0.096	10
Average	0.11	

* Annual release calculated from release rate ($\mu\text{Ci/sec}$) based on 80% plant capacity factor.

TABLE 2-11
COMPARISON BETWEEN IODINE-131 RELEASES FROM REACTOR
BUILDING DURING NORMAL OPERATION AND RELEASES DURING PLANT OUTAGES

FACILITY	NORMAL OPERATION ($\mu\text{Ci/sec}$)	OUTAGES ($\mu\text{Ci/sec}$)	RATIO TOTAL RELEASES* TO NORMAL RELEASES	REFERENCE
Oyster Creek	0.0029	0.014**	2.6	2
Vermont Yankee	0.0038	0.041	3.7	6

* Ratio is based on normal releases occurring 80% of the year and releases during outages occurring 20% of the year.

** Oyster Creek releases include measurements made during drywell purge which was assumed to occur 48 hr/yr.

TABLE 2-12
ANNUAL IODINE-131 RELEASES FROM TURBINE BUILDING VENTILATION
SYSTEMS DURING NORMAL OPERATION

FACILITY	RELEASE (Ci/yr)*	REFERENCE
Vermont Yankee	0.041	6
Oyster Creek	0.61	2
Oyster Creek	0.073	7
Oyster Creek	0.023	7
Millstone 1	0.012	8
Monticello	0.13	2
Dresden 2	0.007	2
Dresden 3	0.015	2
Quad Cities 1	0.012	9
Nine Mile Point 1	0.14	10
Average	0.11	

* Annual release calculated from release rate ($\mu\text{Ci/sec}$) based on 80% plant capacity factor.

TABLE 2-13
COMPARISON BETWEEN IODINE-131 RELEASES FROM TURBINE BUILDING
DURING NORMAL OPERATION AND RELEASES DURING PLANT OUTAGES

FACILITY	NORMAL OPERATION ($\mu\text{Ci/sec}$)	OUTAGES ($\mu\text{Ci/sec}$)	RATIO TOTAL RELEASES* TO NORMAL RELEASES	REFERENCE
Oyster Creek	0.024	0.081**	1.8	2
Vermont Yankee	0.0013	0.0035	1.7	6

* Ratio is based on normal releases occurring 80% of the year and releases during outages occurring 20% of the year.

** Oyster Creek releases include measurements made during drywell purge which was assumed to occur 48 hr/yr.

TABLE 2-14
ANNUAL IODINE-131 RELEASES FROM RADWASTE BUILDING VENTILATION
SYSTEMS, NORMAL OPERATION

<u>FACILITY</u>	<u>RELEASE (Ci/yr)*</u>	<u>REFERENCE</u>
Vermont Yankee	0.057	6
Oyster Creek	0.024	2
Oyster Creek	0.008	7
Nine Mile Point 1	0.008	10
Average	0.024	

*Annual release calculated from release rate ($\mu\text{Ci/sec}$) based on 80% plant capacity factor.

TABLE 2-15
COMPARISON BETWEEN IODINE-131 RELEASES FROM RADWASTE BUILDING
DURING NORMAL OPERATION AND RELEASES DURING PLANT OUTAGES

<u>FACILITY</u>	<u>NORMAL OPERATION ($\mu\text{Ci/sec}$)</u>	<u>OUTAGES ($\mu\text{Ci/sec}$)</u>	<u>RATIO TOTAL RELEASES* TO NORMAL RELEASES</u>	<u>REFERENCE</u>
Oyster Creek	0.00086	0.0031**	1.9	2
Vermont Yankee	0.0018	0.0066	1.9	6

*Ratio is based on normal releases occurring 80% of the year and releases during outages occurring 20% of the year.

**Oyster Creek releases include measurements made during drywell purge which was assumed to occur 48 hr/yr.

The same procedure was used for the radwaste and reactor buildings to obtain total annual iodine-131 releases of 0.046 Ci/yr and 0.34 Ci/yr, respectively. The reactor building releases are based on reactors with a BWR Mark I containment design. Equipment such as the reactor coolant cleanup pumps, residual heat removal system, and emergency core cooling systems have been placed in an auxiliary building in the BWR/6, Mark III containment design concept. Because of the potential for these systems to release radioactive materials from leakage during operation or testing, the Mark I reactor building releases have been assumed to be equally divided between the containment and auxiliary buildings for BWR/6, Mark III designs. The most significant leakage pathway in the turbine building is considered to be through valve stem packings. For this reason, the leakage rate is reduced by a factor of 5 if special design features are applied to reduce or collect leakage from valves in lines 2-1/2 inches in diameter and larger.

The noble gas release rates for building ventilation systems are the average of measurements made at Oyster Creek (Ref. 7) and Millstone Unit 1 (Ref. 8). These data are given in Tables 2-16 through 2-18. The noble gas release rates for the reactor building are equally divided between the containment and auxiliary buildings to reflect the BWR/6, Mark III design.

The radioactive particulate release rates for building ventilation systems are the average of measurements made at Vermont Yankee, Oyster Creek, Dresden 2 & 3, and Nine Mile Point (Refs. 11, 2, and 10). These data are given in Tables 2-21 through 2-27. The calculated annual release rates given above are based on an 80% plant capacity factor, i.e., 80% normal operation at 100% power and 20% plant downtime. To account for differences between release rates during shutdowns of long duration (greater than one week) and those for shorter shutdowns, the 20% downtime of 73 days was assumed to consist of 60 days of long-term shutdowns and 13 days of short-term shutdowns. The releases for normal operation were weighted to account for the operating and shutdown modes in a manner similar to that described previously for iodine releases. The particulate release rates in Tables 2-25 through 2-27 for the radwaste building were measured downstream of HEPA filters and were therefore normalized to upstream concentrations to obtain the radwaste building parameter above. A DF of 15, consistent with HEPA filter DF measurements at Nine Mile Point 1, was used in the normalization (Ref. 10). As described previously for noble gases and iodine, the particulate releases for the reactor building are equally divided between the containment and auxiliary buildings to reflect the BWR/6, Mark III containment design.

2.2.5 IODINE INPUT TO THE MAIN CONDENSER OFFGAS TREATMENT SYSTEM

2.2.5.1 Parameter

The iodine-131 input to the main condenser offgas treatment system, downstream of the air ejectors, is 5 Ci/yr.

2.2.5.2 Bases

Table 2-28 lists the measured iodine-131 releases and integrated thermal power outputs for BWRs with thermal ratings exceeding 1000 Mwt, with more than one year of plant operation and without main condenser offgas treatment. The average ratio of the iodine-131 release in Ci/yr to the integrated thermal power in Mwd for the years 1972, 1973, and 1974 is approximately 5×10^{-6} Ci/Mwd per year. Based on a power rating of 3400 Mwt and an 80% plant capacity factor, the iodine-131 release from the main condenser air ejector is approximately 5 Ci/yr.

2.2.6 TURBINE GLAND SEALING SYSTEM EXHAUST

2.2.6.1 Parameter

Use 0.1% of the main steam flow and assume 99% iodine removal due to radioiodine absorption by condensing steam in the turbine gland seal condenser. If clean steam is supplied to the gland seal, the radioiodine source term is negligible (less than 10^{-4} Ci/yr). If sealing steam is supplied from a low-activity source, i.e., steam produced from demineralized condensate, consider the flow to be zero.

2.2.6.2 Bases

A design value of 0.1% of the main steam flow is used for the turbine gland seal steam flow (Ref. 12). A large fraction of the iodine is expected to be absorbed by the liquid phase during condensation of the gland seal steam. In the absence of radioiodine measurements, it is assumed that the gland seal condenser will remove approximately 99% of the iodine from the noncondensable stream due to iodine adsorption by the condensing water. It is further assumed that the iodine

TABLE 2-16
RELEASES OF NOBLE GASES FROM THE
REACTOR BUILDING VENTILATION SYSTEM
(μ Ci/sec)

NUCLIDE	MILLSTONE		OYSTER CREEK 04/18/72	AVERAGE
	07/21/72	07/24/72		
Kr-85m	0.44	0.07	NR	0.25
Kr-87	0.29	0.19	NR	0.24
Kr-88	0.56	0.20	0.02	0.25
Xe-133	0.67	0.36	15	5.3
Xe-135m	3.0	4.1	NR	3.6
Xe-135	3.1	2.9	2.1	2.7
Xe-138	0.87	NR	0.3	0.6

NR - Not reported.

TABLE 2-17
RELEASES OF NOBLE GASES FROM THE
TURBINE BUILDING VENTILATION SYSTEM
(μ Ci/sec)

NUCLIDE	MILLSTONE	OYSTER CREEK	AVERAGE
	(Ref. 7)	(Ref. 6)	
Kr-85m	2.7	NR	2.7
Kr-87	5.3	NR	5.3
Kr-88	8.2	10	9.1
Xe-133	7.4	12	10
Xe-135m	29	23	26
Xe-135	25	25	25
Xe-138	63	52	58

NR - Not reported.

TABLE 2-18
RELEASES OF NOBLE GASES FROM THE
RADWASTE BUILDING VENTILATION SYSTEM
(μ Ci/sec)

NUCLIDE	MILLSTONE	OYSTER CREEK	AVERAGE
	(Ref. 7)	(Ref. 6)	
Xe-133	0.25	0.56	0.4
Xe-135	2.0	1.5	1.8

TABLE 2-19
 PARTICULATE RELEASE RATES FROM REACTOR BUILDING
 VENTILATION SYSTEM, NORMAL OPERATION (Refs. 40, 2)
 $(10^{-6} \mu\text{Ci/sec})$

NUCLIDE	VERMONT YANKEE	OYSTER CREEK	AVERAGE
Co-60	30	930	480
Co-58	4.6	56	30
Cr-51	5	5.4	5.2
Mn-54	21	370	196
Fe-59	5	47	26
Zn-65	35	11	23
Zr-95	2	NR	2
Sr-89	NA	6.8	6.8
Sr-90	NA	0.3	0.3
Sb-124	NR	11	11
Cs-134	18	18	18
Cs-136	13	NR	13
Cs-137	44	25	35
Ba-140	25	1.8	13
Ce-141	NR	4.3	4.3

NA - Not analyzed.

NR - Not reported.

TABLE 2-20
 PARTICULATE RELEASE RATES FROM REACTOR BUILDING
 VENTILATION SYSTEM, SHORT-TERM SHUTDOWN (2 DAYS/EVENT)(REFS. 11, 2)
 $(10^{-6} \mu\text{Ci/sec})$

NUCLIDE	VERMONT YANKEE*	OYSTER CREEK	AVERAGE
Co-60	104	8100	4100
Co-58	71	37	54
Cr-51	31	37	34
Mn-54	131	23	77
Fe-59	31	37	34
Zn-65	57	19	38
Zr-95	31	NR	31
Sr-89	NA	NA	NA
Sr-90	NA	NA	NA
Sb-124	NR	37	37
Cs-134	51	12000	6030
Cs-136	33	NR	33
Cs-137	97	16000	8050
Ba-140	12	780	396
Ce-141	NR	37	37

NA - Not analyzed.

NR - Not reported.

*Initial drywell purge via SGTS not sampled.

TABLE 2-21
PARTICULATE RELEASE RATES FROM REACTOR BUILDING
VENTILATION SYSTEM, REFUELING SHUTDOWN (REFS. 11, 2)
(10^{-6} $\mu\text{Ci/sec}$)

NUCLIDE	VERMONT YANKEE	OYSTER CREEK	AVERAGE
Co-60	480	590	534
Co-58	77	34	56
Cr-51	120	43	81
Mn-54	55	240	150
Fe-59	21	6	14
Zn-65	1500	2.7	770
Zr-95	150	NR	152
Sr-89	NA	2	2
Sr-90	NA	0.36	0.36
Sb-124	NR	14	14
Cs-134	160	20	90
Cs-136	39	NR	39
Cs-137	380	34	210
Ba-140	27	2	14
Ce-141	NR	11	11

NA - Not analyzed.

NR - Not reported.

TABLE 2-22
PARTICULATE RELEASE RATES FROM TURBINE BUILDING
VENTILATION SYSTEM, NORMAL OPERATION (REFS. 11, 2)
(10^{-6} $\mu\text{Ci/sec}$)

NUCLIDE	VERMONT YANKEE	OYSTER CREEK	DRESDEN 2	DRESDEN 3	AVERAGE
Co-60	3.6	72	4.5	6.0	22
Co-58	2.7	6.7	NR	48	20
Cr-51	NR	840	NR	160	500
Mn-54	1.7	8.4	NR	5	5
Fe-59	NR	6.7	NR	NR	6.7
Zn-65	NR	3.3	NR	NR	3.3
Zr-95	NR	NR	NR	4.0	4.0
Sr-89	NA	610	48	36	230
Sr-90	NA	1.3	0.3	0.25	0.6
Sb-124	NR	6.7	NR	NR	6.7
Cs-134	2.9	15	NR	3.0	7
Cs-136	NR	NR	NR	NR	*
Cs-137	1.9	42	1.8	10	14
Ba-140	133	1400	115	65	430
Ce-141	NR	42	5.5	5	18

NA - Not analyzed.

NR - Not reported.

* Estimated to be less than 1×10^{-6} $\mu\text{Ci/sec}$. A value of 1×10^{-6} $\mu\text{Ci/sec}$ was used to calculate annual release.

TABLE 2-23
PARTICULATE RELEASE RATES FROM TURBINE BUILDING
VENTILATION SYSTEM, SHORT-TERM SHUTDOWN (REFS. 11, 2)
(10^{-6} $\mu\text{Ci/sec}$)

NUCLIDE	VERMONT YANKEE	OYSTER CREEK	AVERAGE
Co-60	5.5	46	26
Co-58	1.5	46	24
Cr-51	NR	46	46
Mn-54	3.5	15	9.2
Fe-59	NR	46	46
Zn-65	NR	23	23
Zr-95	NR	NR	*
Sr-89	NA	NA	NA
Sr-90	NA	NA	NA
Sb-124	NR	46	46
Cs-134	1.8	170	86
Cs-136	NR	NR	*
Cs-137	4.5	240	120
Ba-140	25	110	68
Ce-141	NR	46	46

NA - Not analyzed.

NR - Not reported.

* Estimated to be less than 10^{-6} $\mu\text{Ci/sec}$. A value of 1×10^{-6} $\mu\text{Ci/sec}$ was used to calculate annual release.

TABLE 2-24
PARTICULATE RELEASE RATES FROM TURBINE BUILDING
VENTILATION SYSTEM, REFUELING SHUTDOWN (REFS. 11, 2)

(10^{-6} $\mu\text{Ci/sec}$)

NUCLIDE	VERMONT YANKEE	OYSTER CREEK	AVERAGE
Co-60	3.5	490	250
Co-58	1	29	15
Cr-51	NR	72	72
Mn-54	1	180	90
Fe-59	NR	49	49
Zn-65	NR	11	11
Zr-95	NR	NR	*
Sr-89	NA	2.5	2.5
Sr-90	NA	0.25	0.25
Sb-124	NR	9.5	9.5
Cs-134	2.5	26	14
Cs-136	NR	NR	*
Cs-137	5	57	31
Ba-140	3.6	3.4	3.5
Ce-141	NR	20	20

NA - Not analyzed.

NR - Not reported.

* Estimated to be less than 10^{-6} $\mu\text{Ci/sec}$. A value of 1×10^{-6} $\mu\text{Ci/sec}$ was used to calculate annual release.

TABLE 2-25
PARTICULATE RELEASE RATE* FROM RADWASTE BUILDING
VENTILATION SYSTEM, NORMAL OPERATION (REFS. 11, 2, 8)
(10^{-6} $\mu\text{Ci/sec}$)

NUCLIDE	VERMONT YANKEE	OYSTER CREEK	NINE MILE POINT	AVERAGE
Co-60	0.7	55	83 **	46
Co-58	0.64	1.5	2.0	1.4
Cr-51	NR	5.3	NR **	5.3
Mn-54	0.43	14	8.7 **	7.7
Fe-59	NR	0.72	NR	0.72
Zn-65	1	0.63	NR	0.82
Zr-95	NR	NR	NR	***
Sr-89	NA	0.72	NR	0.72
Sr-90	NA	0.72	NR	0.72
Sb-124	NR	NR	NR	***
Cs-134	0.8	3	33	12
Cs-136	1	NR	NR	1
Cs-137	1.9	6.8	57	22
Ba-140	3.7	NR	NR	3.7
Ce-141	NR	0.72	NR	0.72

NR - Not reported.

NA - Not analyzed.

* Downstream of HEPA filters.

** Calculated based on known filter inlet activity concentration using DF of 15.

*** Estimated to be less than 1×10^{-6} $\mu\text{Ci/sec}$. A value of 1×10^{-6} was used to calculate annual release.

TABLE 2-26
PARTICULATE RELEASE RATE* FROM RADWASTE BUILDING
VENTILATION SYSTEM, SHORT-TERM SHUTDOWN (REFS. 11, 2)
(10^{-6} $\mu\text{Ci/sec}$)

NUCLIDE	VERMONT YANKEE	OYSTER CREEK	AVERAGE
Co-60	1.1	68	35
Co-58	0.95	7.2	4.1
Cr-51	NR	7.2	7.2
Mn-54	0.64	19	9.8
Fe-59	NR	7.2	7.2
Zn-65	1	4.3	2.7
Zr-95	NR	NR	**
Sr-89	NA	NA	NA
Sr-90	NA	NA	NA
Sb-124	NR	NR	**
Cs-134	1.3	7.2	4.3
Cs-136	1.1	NR	1.1
Cs-137	8.6	7.2	8.0
Ba-140	0.92	NR	0.92
Ce-141	NR	7.2	7.2

NA - Not analyzed.

NR - Not reported.

* Downstream of HEPA filters.

** Estimated to be less than 10^{-6} $\mu\text{Ci/sec}$. A value of 1×10^{-6} $\mu\text{Ci/sec}$ was used to calculate annual release.

TABLE 2-27
 PARTICULATE RELEASE RATE* FROM RADWASTE BUILDING
 VENTILATION SYSTEM, REFUELING SHUTDOWN (REFS. 11, 2)
 $(10^{-6} \mu\text{Ci/sec})$

NUCLIDE	VERMONT YANKEE	OYSTER CREEK	AVERAGE
Co-60	0.8	1850	920
Co-58	0.6	114	57
Cr-51	NR	92	92
Mn-54	0.6	860	430
Fe-59	NR	250	250
Zn-65	1	29	15
Zr-95	NR	NR	**
Sr-89	NA	1.8	1.8
Sr-90	NA	0.08	0.08
Sb-124	NR	NR	**
Cs-134	1	15	8
Cs-136	1	NR	1
Cs-137	3.9	34	19
Ba-140	1.1	NR	1.1
Ce-141	NR	29	29

NR - Not reported.

NA - Not analyzed.

* Downstream of HEPA filters

** Estimated to be less than $10^{-6} \mu\text{Ci/sec}$. A value of $1 \times 10^{-6} \mu\text{Ci/sec}$ was used to calculate annual release.

TABLE 2-28
IODINE-131 RELEASES FROM THE MAIN CONDENSER AIR EJECTORS*

FACILITY	1972			1973			1974		
	IODINE RELEASE (Ci/yr)	INTEGRATED THERMAL POWER (10 ⁶ MWD)	Ci/yr 10 ⁶ MWD	IODINE RELEASE (Ci/yr)	INTEGRATED THERMAL POWER (10 ⁶ MWD)	Ci/yr 10 ⁶ MWD	IODINE RELEASE (Ci/yr)	INTEGRATED THERMAL POWER (10 ⁶ MWD)	Ci/yr 10 ⁶ MWD
Oyster Creek	6.3	0.542	12.0	6.7	0.453	14.0	3.3	0.46	7.2
Nine Mile Point 1	0.89	0.417	2.0	1.9	0.457	4.4	0.7	0.43	1.7
Millstone 1	1.2	0.404	3.0	0.15	0.248	0.6	0.29	0.47	0.6
Dresden 2, 3**	5.1	1.05	4.6	9.8	1.18	8.3	4.0	0.91	4.4
Monticello	0.58	0.454	1.3	1.2	0.413	2.9	5.7	0.34	17.0
Pilgrim 1			***	0.46	0.523	0.9	1.4	0.25	5.8
Quad Cities 1, 2**			***	5.5	1.32	4.2	8.2	1.09	7.5
Average			4.5			5.4			6.2

Combined average for 1972, 1973, 1974 -- $5.4 \times 10^{-6} \frac{\text{Ci/yr}}{\text{MWD}}$

* Data from semiannual operating for 1972, 1973, 1974 for facilities listed.

** Two-unit plants with a single stack.

*** Not included in 1972 average because plants had not achieved a full year of operation.

source term is negligible when clean steam (nonradioactive steam from an auxiliary steam supply system) is used for the gland seal. Because of noble gas removal in the main condenser, iodine removal by the condensate demineralizers, and partitioning in the boiler, steam produced from demineralized condensate is considered to be clean steam. Data in Tables 2-29 and 2-30 show the release of radioactive particulates from the turbine gland seal to be negligible.

TABLE 2-29
PARTICULATE RELEASE RATE FROM VERMONT YANKEE MECHANICAL VACUUM PUMP AND GLAND EXHAUST CONDENSER VENT,
SHORT-TERM SHUTDOWN

NUCLIDE	RELEASE RATE (10^{-6} $\mu\text{Ci/sec}$)
Cs-134	1.2
Cs-136	1.1
Cs-137	4.9
Ba-140	2.9

TABLE 2-30
PARTICULATE RELEASE RATE FROM VERMONT YANKEE VACUUM PUMP AND GLAND EXHAUST CONDENSER VENT, REFUELING SHUTDOWN

NUCLIDE	RELEASE RATE (10^{-6} $\mu\text{Ci/sec}$)
Cs-134	0.45
Cs-136	0.13
Cs-137	1.0
Ba-140	1.6

2.2.7 MAIN CONDENSER MECHANICAL VACUUM PUMP

2.2.7.1 Parameter

Xe-133	2300 Ci/yr per reactor
Xe-135	350 Ci/yr per reactor
I-131	0.03 Ci/yr per reactor

2.2.7.2 Bases

The release values for Xe-133 and Xe-135 were derived from Dresden 1 operating data (Ref. 13). These data indicate that approximately 580 Ci of Xe-133 and 85 Ci of Xe-135 were released with the Dresden 1 mechanical vacuum pump effluent when establishing main condenser vacuum following a plant shutdown. At the point in the fuel cycle where the data were taken, the reactor was operating at an offgas rate of approximately 60,000 $\mu\text{Ci/sec}$.

The release value for iodine-131 was derived from operating data taken at Vermont Yankee (Ref. 6). These data indicate that the release rate for iodine-131 due to mechanical vacuum pump operation during plant startup was approximately 0.09 $\mu\text{Ci/sec}$. Information from reactor operators indicates that the mechanical vacuum pumps are operated periodically during plant shutdowns to maintain a slight condenser vacuum and prevent leakage from the condenser to the turbine building. A total of 24 hours of vacuum pump operation per shutdown was assumed for purposes of calculating iodine releases. The annual release estimates for noble gases and iodine-131 are based on four shutdowns per year. Data in Tables 2-29 and 2-30 show the release of radioactive particulates from the mechanical vacuum pump to be negligible.

2.2.8 AIR INLEAKAGE TO THE MAIN CONDENSER

2.2.8.1 Parameter

10 ft³/min air inleakage for each condenser shell of the main condenser.

2.2.8.2 Bases

Air inleakage to the main condenser is a function of the number of condenser shells and of the station housekeeping performed to reduce inleakage and maintain low inleakage levels. Operating data for inleakage vary widely. For example, Oyster Creek and Dresden 2 air inleakage measurements during early operation indicated that leakage rates were 4 to 250 ft³/min. Yet, Dresden 1 inleakage during full-power operation has been measured to be approximately 3 ft³/min.

A large amount of air inleakage data has been evaluated for TVA power plants, where inleakage measurements have been recorded for several years. Air inleakage measurements for six TVA plants, representing more than 40 years of cumulative experience, indicate leakage rates ranging from 4 to 12 ft³/min per condenser shell.

An air leakage rate of 10 ft³/min per condenser shell is assumed for nuclear power plants under normal operating conditions, including anticipated operational occurrences, averaged over the life of the plant.

2.2.9 HOLDUP TIMES FOR CHARCOAL DELAY SYSTEMS

2.2.9.1 Parameter

$$T = 0.26 MK/10 N$$

where

K is the dynamic adsorption coefficient, in cm³/g (see chart below);

M is the mass of charcoal adsorber, in thousands of pounds;

T is the holdup time, in hours; and

10 N is the number of shells in main condenser times 10 ft³/min inleakage per shell.

Dynamic adsorption coefficients (in cm³/g) are as follows:

	OPERATING 77°F DEW POINT 45°F	OPERATING 77°F DEW POINT 0°F	OPERATING 0°F DEW POINT -20°F
Kr	18.5	25	105
Xe	330	440	2410

2.2.9.2 Bases

Charcoal delay systems are evaluated using the above equation and dynamic adsorption coefficients. $T = MK/10 N$ is a standard equation for the calculation of delay times in charcoal adsorption systems (Ref. 14). The dynamic adsorption coefficients (K values) for Xe and Kr are dependent on operating temperature and moisture content (Refs. 15 and 16) in the charcoal, as indicated by the values in the above parameter. The K values represent a composite of data from operating reactor charcoal delay systems (Refs. 17 and 18) and reports concerning charcoal adsorption systems (Refs. 14, 15, 16, 18, 19, 20, and 21).

The factors influencing the selection of K values are

1. Operational data from KRB* (Kr = 20-30, K_{Xe} = 260-430) (Ref. 17) and from KWL** (K_{Kr} = 30, K_{Xe} = 500)

* Kernkraftwerk RWE - Bayernwerk GmbH.

** Kernkraftwerk Lingen GmbH.

2. The effect of temperature on the dynamic adsorption coefficients, indicated in Figure 2-2 (Ref. 15).
3. The effect of moisture on the dynamic adsorption coefficients, shown in Figure 2-3. The affinity of charcoal for moisture, shown in Figure 2-4.
4. The variation in K values between researchers and between the types of charcoal used in these systems (Refs. 15, 22, and 23). Because of the variation in K values based on different types of charcoal and the data reported, average values taken from KRB and KWL data shown in Figure 2-2 are used.

The coefficient 0.26 adjusts the units and was calculated as follows:

$$T(\text{hr}) = \frac{M(10^3 \text{ lb}) K(\text{cm}^3/\text{g})(454 \text{ g/lb})(3.53 \times 10^{-5} \text{ ft}^3/\text{cm}^3)}{(10 \text{ ft}^3/\text{min-shell})(N \text{ shells})(60 \text{ min/hr})}$$

$$T = 0.26 \frac{MK}{10 N}$$

2.2.10 DECONTAMINATION FACTORS FOR CRYOGENIC DISTILLATION

2.2.10.1 Parameter

<u>NUCLIDES</u>	<u>DECONTAMINATION FACTOR</u>
I, Xe	1×10^4
Kr	4×10^3

The holdup times are calculated on the basis of gas residence time in the system prior to release.

2.2.10.2 Bases

A DF of 10^4 for iodine and xenon and a DF of 4×10^3 for krypton are used for a cryogenic distillation system. The values are based on data submitted in Amendment 11 to the PSAR for the Hope Creek Nuclear Generating Station, Units 1 and 2 (Ref. 24), which were derived from a proprietary report (Ref. 25) of Air Products and Chemical, Inc. The PSAR states that a maximum of 0.025% Kr (DF = 4×10^3) and 0.01% Xe (DF = 10^4) will escape from the system. These decontamination factors are considered reasonable.

2.2.11 DECONTAMINATION FACTOR FOR THE CHARCOAL ADSORBERS AND HEPA FILTERS

2.2.11.1 Parameter

Use a nominal DF of 10 for iodine removal by charcoal adsorbers subject to applicant's commitment to provide data to support charcoal bed depth for removal efficiency used. Use a DF of 100 for particulate removal by HEPA filtration.

2.2.11.2 Bases

Only very limited data are available concerning the removal of iodine at trace concentrations ($10^{-12} \mu\text{Ci/cm}^3$). The majority of the available data concerning iodine adsorption on activated carbon is addressed toward iodine concentrations that are orders of magnitude higher than the levels of concern in source term evaluations for normal operations.

The iodine removal efficiency of activated carbon varies greatly, even between carbon in the same lot (Ref. 23). This lack of consistency makes the comparison of reported data difficult. The difficulty is compounded by sampling and measurement problems encountered when working with the low iodine concentrations involved. Accordingly, useful information concerning the adsorption of trace quantities of iodine is limited (Ref. 26). In addition, when iodine is present in low concentrations, impurities in the carrier gas may be adsorbed by the charcoal causing competition between the iodine and impurities. Over long periods of time (i.e., several months), such impurities may saturate (poison) the adsorber (Ref. 27), thereby decreasing the apparent iodine adsorption coefficient (Ref. 26) and shortening the time before iodine breakthrough. Channeling through the charcoal bed via passages caused by poor initial bed packing or by settling during use will also decrease adsorber efficiency.

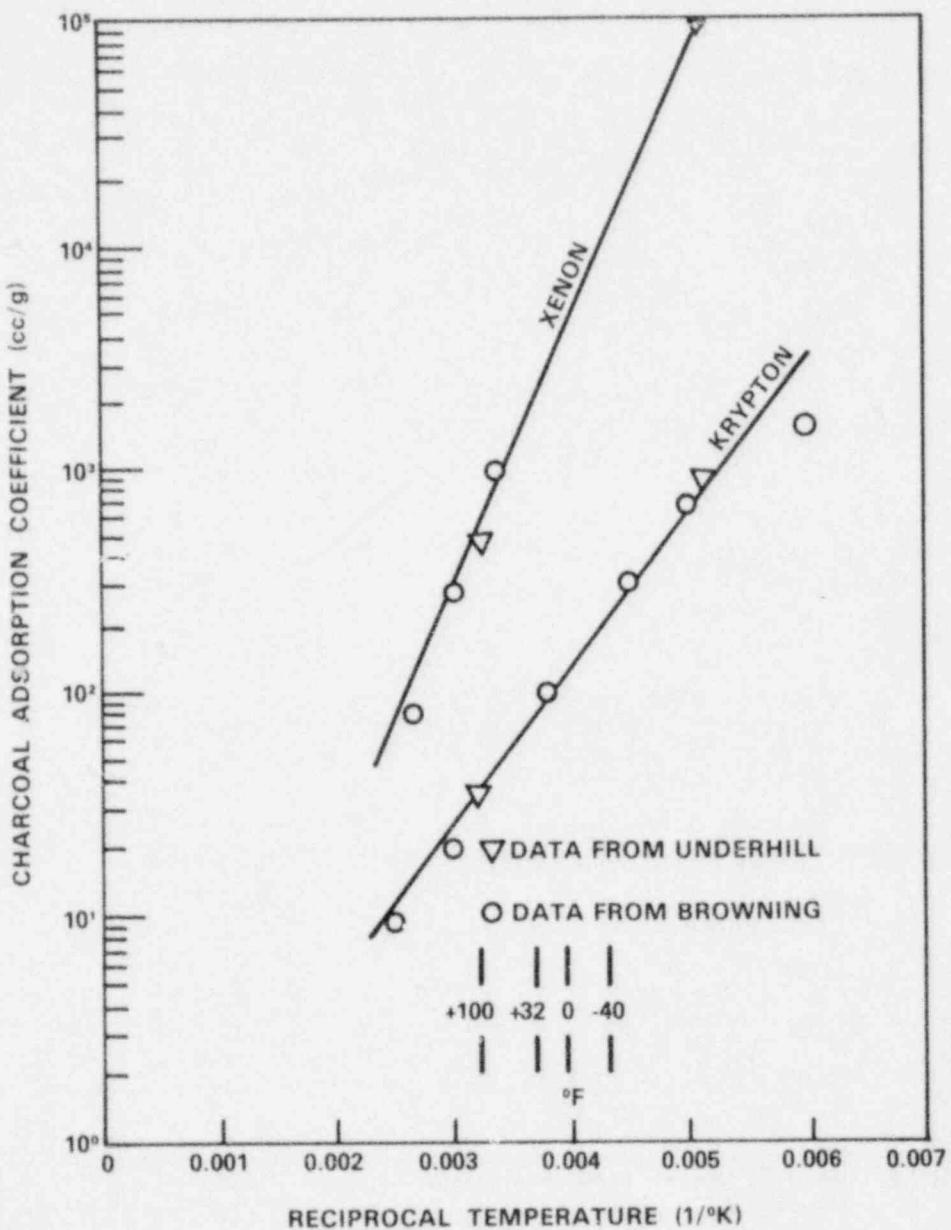


FIGURE 2-2
KRYPTON AND XENON K VALUES AS A FUNCTION
OF RECIPROCAL TEMPERATURE

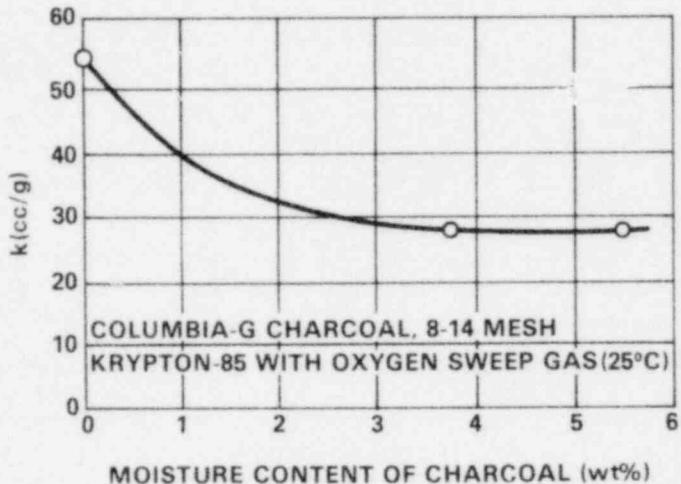


FIGURE 2-3
EFFECT OF MOISTURE CONTENT ON THE
DYNAMIC ADSORPTION COEFFICIENT

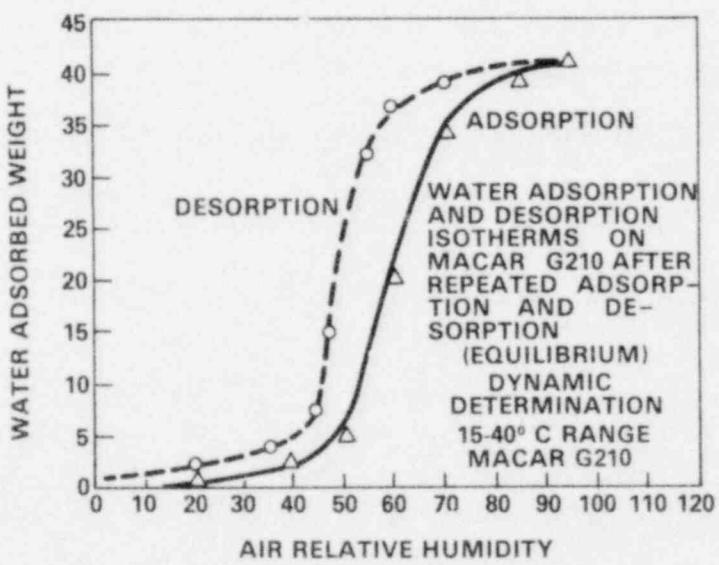


FIGURE 2-4
CHARCOAL MOISTURE AS A FUNCTION
OF RELATIVE HUMIDITY

Data being developed for iodine removal at trace levels may be used by applicants to substantiate the iodine removal efficiencies. The DF of 100 for HEPA filters is consistent with expected particulate removal efficiencies under normal operating conditions.

The DF assigned the charcoal adsorbers and HEPA filters considers in-place leak testing to be conducted before use and routinely thereafter, as recommended in ANSI Standard N510, "Testing of Nuclear Air Cleaning Systems" (Ref. 28).

2.2.12 LIQUID WASTE INPUTS

2.2.12.1 Parameter

The flow rates listed in Table 2-31 are used as inputs to the liquid radwaste treatment system. Flows that cannot be standardized are added to those listed in Table 2-31 to fit an individual application. Disposition of liquid streams to the appropriate collection tanks is based on the applicant's intended method of processing.

2.2.12.2 Bases

The liquid waste inputs are based on the values proposed by the ANS 52.3 Working Group draft standard for boiling water reactor liquid radwaste system (Ref. 29). Activity inputs are based on the reactor coolant concentrations proposed by ANS 18.1 Working Group draft standard (Ref. 1) boiling water reactor source terms given in Parameter 2.2.3. The values given are those that were judged to be representative for a typical BWR design.

2.2.13 CHEMICAL WASTES FROM REGENERATION OF CONDENSATE DEMINERALIZERS

2.2.13.1 Parameter

1. Liquid flows to demineralizer at main steam activity.
2. All nuclides removed from the reactor coolant by the demineralizers are removed from the resins during regeneration.
3. Use a regeneration cycle of 3.5 days times the number of demineralizers. (For systems using ultrasonic resin cleaning, use 7 days times the number of demineralizers.)

2.2.13.2 Bases

Operating data from Dresden 2 and 3 indicate that one condensate demineralizer regeneration occurs every 3.5 days (Ref. 30).

All material exchanged or filtered out by the resins between regenerations is contained in the regenerant waste streams; therefore, each regeneration will have approximately the same effectiveness (i.e., each regeneration removes all material collected since the previous regeneration, leaving a constant quantity of material on the resins after regeneration). Regeneration cycles are normally controlled by particulate buildup on resin beds, resulting in high pressure drops across the bed. If ultrasonic resin cleaning is used to remove insolubles between regenerations, the effective bed life between regenerations will be approximately doubled based on preliminary operating data from Dresden and Pilgrim 1 (Refs. 31 and 32).

2.2.14 DETERGENT WASTE

2.2.14.1 Parameter

For plants with an onsite laundry, use 450 gal/day per reactor of detergent waste and the radionuclide distribution given in Table 2-32 for untreated detergent wastes. The quantities shown in Table 2-32 are added to the adjusted liquid source term. They are reduced for any treatment provided using the appropriate decontamination factors.

2.2.14.2 Bases

In the evaluation of liquid radwaste treatment systems, it is assumed that detergent wastes (laundry drains, personnel and equipment decontamination drains, and cask cleaning drains) will total approximately 450 gal/day per reactor. The radionuclide distribution given in Table 2-32 is based on data from Ginna given in Table 2-33.

TABLE 2-31
BWR LIQUID WASTES

SOURCE	PLANT WITH ULTRASONIC RESIN CLEANER	PLANT WITHOUT ULTRASONIC RESIN CLEANER	FLOW RATE (gal/day)	FRACTION OF PRIMARY COOLANT ACTIVITY (PCA)
<u>Equipment Drains</u>				
Drywell	3,400	3,400		1
Containment, auxiliary building, and fuel pool	3,720	3,720		0.01
Radwaste building	1,060	1,060		0.01
Turbine building	2,960	2,960		0.01
Ultrasonic resin cleaner*	15,000	-		0.05
Resin rinse	2,500	5,000		0.002
Subtotal	28,640	16,140		-
<u>Floor Drains</u>				
Drywell	700	700		1
Containment, auxiliary building, and fuel pool	2,000	2,000		0.01
Radwaste building	1,000	1,000		0.01
Turbine building	2,000	2,000		0.01
Subtotal	5,700	5,700		-
<u>Other</u>				
Cleanup phase separator decant	640	640		0.002
Laundry drains	450	450		**
Lab drains	500	500		0.02
Regenerants*	1,700	3,400		***
Condensate backwash ⁺	-	8,100		2×10^{-6}
Chemical lab waste	100	100		0.02
Total	37,730	26,930		

* - Deep-bed condensate demineralizers.
** - Listed in BWR-GALE Code, see Table 2-32.

*** - Calculated by BWR-GALE Code.
+ - Filter/demineralizer (Powdex) condensate demineralizer.

TABLE 2-32
CALCULATED ANNUAL RELEASE OF RADIOACTIVE MATERIALS IN
UNTREATED DETERGENT WASTE FROM A BWR AND PWR

<u>NUCLIDE</u>	<u>Ci/yr</u>
Mn-54	0.001
Co-58	0.004
Co-60	0.009
Zr-95	0.0014
Nb-95	0.002
Ru-103	0.00014
Ru-106	0.0024
Ag-110m	0.00044
I-131	0.0006
Cs-134	0.013
Cs-137	0.024
Cs-144	<u>0.005</u>
Total	~0.06

TABLE 2-33
 GINNA NUCLEAR POWER STATION
 RADIONUCLIDE DISTRIBUTION OF DETERGENT WASTE
 FOR PERIOD OCTOBER 1972 - JULY 1973 (Ref. 33)

NUCLIDE	10/26/72 to 11/25/72	11/26/72 to 12/31/72	1/01/73 to 1/31/73	2/01/73 to 2/28/73	3/01/73 to 3/31/73	4/01/73 to 4/30/73	5/01/73 to 5/31/73	6/01/73 to 6/30/73	7/01/73 to 7/31/73	MONTHLY AVG.	MAX.	MIN.
Cs-137	2.93	0.87	0.31	1.02	1.59	12.8	0.55	0.48	1.58	2.46	12.8	0.31
Cs-134	2.04	0.48	0.19	0.53	0.82	7.0	0.26	0.21	0.60	1.35	7.0	0.19
Co-60	1.04	1.04	0.24	0.92	0.86	2.1	0.23	0.16	1.54	0.90	2.1	0.16
Co-58	0.82	0.74	0.10	0.17	1.32	0.43	0.08	0.02	0.03	0.47	1.3	0.02
Mn-54	-	0.21	0.05	0.12	0.11	0.25	0.06	-	0.15	0	0.25	0.05
Zr-95	0.59	0.25	0.07	0.09	0.10	0.17	-	-	-	0.14	0.59	0.07
Nb-95	0.49	0.39	0.09	0.16	0.17	0.35	0.06	-	0.11	0.20	0.49	0.06
I-131	-	-	-	-	-	-	-	-	0.06	0.06	0.06	-
Ce-144	1.05	0.76	0.17	0.55	0.43	1.50	0.26	0.08	0.41	0.53	1.50	0.08
Ce-141	-	-	0.01	-	-	-	-	-	-	0.001	0.01	-
Ru-106	1.91	-	0.30	-	-	-	-	-	-	0.25	1.9	0.30
Ru-103	-	-	0.02	0.019	0.09	-	-	-	-	0.014	0.09	0.23
Ag-110m	-	-	0.08	0.02	0.07	0.23	-	-	-	0.05	0.23	0.02
Cr-51	-	-	-	-	-	-	-	-	-	-	-	-
Mo-99	-	-	-	0.005	-	-	-	-	-	0.005	0.005	-
Total	10.9	4.7	1.6	3.4	5.6	24.8	1.5	0.9	4.5	6.4	24.8	0.94
Monthly Flow (gal)	24,380	6,770	1,800	10,680	10,290	8,620	5,220	3,400	5,200	8,420	24,380	1,800
Daily Flow (gal)	-	-	-	-	-	-	-	-	-	280	810	60

2.2.15 TRITIUM RELEASES

2.2.15.1 Parameter

The total tritium release through liquid and vapor pathways is 0.025 Ci/yr per Mwt. The quantity of tritium released through the liquid pathway is based on the calculated volume of liquid released with a tritium concentration of 0.01 uCi/cm³ up to a maximum of 50% of the total quantity of tritium calculated to be available for release. The remainder of the tritium produced is assumed to be released as a vapor from the plant vent.

2.2.15.2 Bases

Table 2-34 lists the measured liquid and gaseous tritium releases from BWRs for 1972, 1973, and 1974. Based on the total tritium release for each facility, the integrated thermal power produced during the year, and a plant capacity factor of 80%, the total annual release is approximately 0.025 Ci/Mwt through the combined liquid and vapor pathways.

The tritium can be released either in liquid wastes or as a vapor with ventilation effluents, the relative amounts being dependent on liquid recycle practices. The tritium concentration assumed for the liquid releases is based on the tritium concentration given in Table 2-2 and is the value recommended by the ANS 18.1 Working Group for BWR source term calculations. This value is based on a review of tritium concentrations in BWR liquid streams (Ref. 1). This evaluation assumes steady-state conditions; i.e., the tritium inventory in the plant remains constant and the tritium entering the reactor water is released through the liquid and vapor pathways.

2.2.16 DECONTAMINATION FACTORS FOR DEMINERALIZERS

2.2.16.1 Parameter

The following are the expected decontamination factors (DFs) for demineralizers used on process or radwaste streams.

DEMINERALIZER TYPE	DECONTAMINATION FACTORS*		
	ANION	Cs, Rb	OTHER NUCLIDES
<u>Mixed Bed ($H^+ OH^-$)</u>			
Reactor coolant	10	2	10
Condensate	10	2	10
Clean waste	$10^2(10)$	10(10)	$10^2(10)$
Dirty waste (floor drains)	$10^2(10)$	2(10)	$10^2(10)$
<u>Cation Bed (H^+)</u>			
Dirty waste	1(1)	10(10)	$10^2(10)$
Powdex (any system)	10(10)	2(10)	10(10)

* For an evaporator polishing demineralizer or for the second demineralizer in series, the DF is given in the parentheses.

2.2.16.2 Bases

The DFs for demineralizers used in the evaluation of liquid waste treatment systems are derived from the findings of a generic review in the nuclear industry by ORNL (Ref. 34). This reference contains operating and theoretical data that provide a basis for the numerical values assigned. The information contained in this report was projected to obtain a performance value expected over an extended period of operation. It was also considered that attempts to extend the service life of the resin will reduce the DFs below those expected under controlled operating conditions.

TABLE 2-34
TRITIUM RELEASE DATA FROM OPERATING BWRS*

REACTOR NAME	POWER (Mwt)	STARTUP DATE	NUCLEAR THERMAL OUTPUT (10 ⁶ MWdt)			TRITIUM RELEASED (Ci/yr)						RATIO OF TOTAL TRITIUM RELEASED (Ci/yr-Mwt at 80% capacity)		
			1972	1973	1974	1972	1973	1974	1972	1973	1974	1972	1973	1974
Dresden 1	700	1959	0.16	0.10	0.05	**	**	**	43	18.5	18.8	0.078	0.054	0.11
Oyster Creek	1930	1969	0.54	0.45	0.46	0.8	0.4	0.4	62	36.6	14.1	0.034	0.024	0.009
Nine Mile Point	1850	1969	0.42	0.46	0.44	18	26.8	**	28	46.5	18.7	0.032	0.047	0.012
Dresden 2, 3	2577	1970/71	1.04	1.18	0.91	31	10	11	26	26	22.6	0.016	0.009	0.011
Millstone 1	2011	1970	0.40	0.25	0.47	4.2	1.7	2.8	21	3.7	24.1	0.018	0.006	0.017
Monticello	1670	1970	0.46	0.41	0.37	12	**	**	***	***	***	0.008	-	-
Vermont Yankee	1593	1972	0.06	0.18	0.34	+	1.0	0.9	+	0.2	**	-	0.002	0.001
Quad Cities 1, 2	2511	1971/72	0.52	1.32	1.09	4.7	34 ^{††}	29	4.7	24.5	34	0.005	~0.013	0.017
Pilgrim 1	1998	1972	0.11	0.53	0.25	**	14	8	4.2	0.4	10.5	0.011	0.008	0.022
Average												0.025	~0.020	0.025

2-37

* Data from semiannual reports of reactors listed.

** No reported data.

*** No measurement made.

[†]Prior to first core refueling.

^{††}Measured only during the July-December 1973 period.

The following operating conditions were factored into the evaluation of demineralizer performance:

1. In general, the DF for waste treatment systems will vary with the quality of the water to be treated, increasing with increasing activity. Normally, when two demineralizers are used in series, the first demineralizer will have a higher DF than the second. However, the data in Reference 34 indicate that Cs and Rb will be more strongly exchanged in the second demineralizer in series than in the first, since the concentration of preferentially exchanged competing nuclides is reduced.

2. As indicated in Reference 34, compounds of Y, Mo, and Tc form colloidal particles that tend to plate out on solid surfaces. Mechanisms such as plateout on the relatively large surface area provided by demineralizer resin lead to removal of these nuclides to the degree stated above. An analysis of effluent release data indicates that these nuclides, although present in the primary coolant, are normally undetectable in the effluent streams.

2.2.17 DECONTAMINATION FACTORS FOR EVAPORATORS

2.2.17.1 Parameter

	<u>ALL NUCLIDES EXCEPT IODINE</u>	<u>IODINE</u>
Miscellaneous radwaste evaporator	10^4	10^3
Separate evaporator for detergent wastes	10^2	10^2

2.2.17.2 Bases

The decontamination factors for evaporators are derived from the findings of a generic review by ORNL of evaporators used in the nuclear industry (Ref. 35). The principal conclusions reached in the report are

1. Decontamination factors of 10^4 can be expected for nonvolatile radioactive nuclides in a single-stage evaporator.
2. Decontamination factors for iodine are a factor of 10 less than the DFs for non-volatile nuclides.
3. Decontamination factors for wastes containing detergents that tend to foam are a factor of 10 to 100 lower than DFs expected for nonfoaming wastes.

These conclusions have been extended to take into account the following factors:

1. For nonvolatile nuclides in a nonfoaming solution, a DF of 10^4 is used.
2. If an evaporator is used for detergent wastes, the DF for the evaporator is reduced to 100 to reflect carryover due to foaming, which will reduce the DF.

2.2.18 DECONTAMINATION FACTORS FOR REVERSE OSMOSIS

2.2.18.1 Parameter

Overall DF of 30 for laundry wastes and DF of 10 for other liquid radwastes.

2.2.18.2 Bases

Reverse osmosis processes are generally run as semibatch processes. The concentrated stream rejected by the membrane is recycled until a desired fraction of the batch is processed through the membrane. The ratio of the volume processed through the membrane to the inlet batch volume is the percent recovery. The DF normally specified for the process is the ratio of nuclide concentrations in the concentrated liquor stream to the concentrations in the effluent stream. This ratio is termed as the membrane DF. For source term calculations, the system DF should be used. The system DF is the ratio of the nuclide concentrations in the feed stream to those in the effluent stream. The relationship between the system DF and the membrane DF is nonlinear and is a function of the percent recovery. This relationship can be expressed as follows:

$$DF_s = \frac{F}{1 - [1 - F]^{1/DF_m}}$$

where

DF_m is the membrane DF;

DF_s is the system DF; and

F is the ratio of effluent volume to inlet volume (percent recovery).

Tables 2-35 through 2-37 give membrane DFs derived from operating data at Point Beach and Ginna (Refs. 36, 37, 38, and 39) and laboratory data on simulated radwaste liquids (Refs. 40 and 41). These data indicate that the overall membrane DF is approximately 100. The percent recovery for liquid radwaste processes using reverse osmosis is expected to be approximately 95%, i.e., 5% concentrated liquor. Using these values in the above equation, the system DF is approximately 30.

$$DF_s = \frac{0.95}{1 - (1 - .95)^{1/100}} = 30$$

The data used were derived mainly from tests on laundry wastes. The DF for other plant wastes, e.g., floor drain wastes, is expected to be lower because of the higher concentrations of iodine and cesium isotopes. As indicated by the data in Tables 2-35 and 2-37, the membrane DF for these isotopes is lower than the average membrane DF used in the evaluation for laundry waste.

2.2.19 GUIDELINES FOR CALCULATING LIQUID WASTE HOLDUP TIMES

The radioactive-decay holdup times applied to the input waste streams are calculated using the following parameters:

1. The collection time for an 80% volume change in the tank, based on the liquid waste flow rates from the source (above values).
2. The total time liquid remains in the system for processing, based on the flow rate through the limiting process step.
3. One-half the time required to empty the final liquid waste sample (test) tank to the environment. This value is based on the maximum rate of the discharge pumps and the nominal tank volume.

The calculated values in 1. and the total of 2. and 3. are used as inputs to the computer code.

2.2.20 ADJUSTMENT TO LIQUID RADWASTE SOURCE TERMS FOR ANTICIPATED OPERATIONAL OCCURRENCES

2.2.20.1 Parameter

1. Increase the calculated source term by 0.15 Ci/yr per reactor using the same isotopic distribution as for the calculated source term to account for anticipated operational occurrences such as operator errors that result in unplanned releases.

2. Assume evaporators to be unavailable for two consecutive days per week for maintenance. If a 2-day holdup capacity or an alternative evaporator is available, no adjustment is needed. If less than a 2-day capacity is available, assume the waste excess is handled as follows:

a. High-purity or low-purity waste - Processed through an alternative system (if available) using a discharge fraction consistent with the lower purity system.

b. Chemical Waste - Discharged to the environment to the extent holdup capacity or an alternative evaporator is unavailable.

2.2.20.2 Bases

Reactor operating data over a 2-1/2-year period January 1973 through June 1975, representing 102 reactor years of operation were evaluated to determine the frequency and extent of

TABLE 2-35
REVERSE OSMOSIS DECONTAMINATION FACTORS, GINNA STATION (REF. 36)

NUCLIDE	CONCENTRATE ACTIVITY ($\mu\text{Ci}/\text{cm}^3$)	PRODUCT ACTIVITY ($\mu\text{Ci}/\text{cm}^3$)	MEMBRANE DF
Ce-144	2.88×10^{-4}	$<2.2 \times 10^{-7}$	1200
Co-58	8.55×10^{-5}	$<3.4 \times 10^{-8}$	1600
Ru-103	5.83×10^{-5}	$<5.5 \times 10^{-8}$	1100
Cs-137	4.09×10^{-4}	6.6×10^{-6}	60
Cs-134	2.02×10^{-4}	3.2×10^{-6}	60
Nb-95	5.35×10^{-5}	$<5.3 \times 10^{-8}$	1000
Zr-95	2.36×10^{-5}	$<3.7 \times 10^{-8}$	640
Mn-54	8.82×10^{-5}	$<3.4 \times 10^{-8}$	2600
Co-60	9.62×10^{-4}	$<8.1 \times 10^{-8}$	12,000
Total isotopic	2.15×10^{-3}	9.8×10^{-6}	220
Gross β	1.63×10^{-3}	1.86×10^{-5}	88
Total isotopic - Weak β	1.93×10^{-3}	9.8×10^{-6}	<u>192</u>
Average*			200

*The average DF is calculated from the average of the reciprocals of the isotopic DFs.

TABLE 2-36
REVERSE OSMOSIS DECONTAMINATION FACTORS, POINT BEACH (REF. 39)

DATE	TIME	FEED ACTIVITY ($\mu\text{Ci}/\text{ml}$)	PRODUCT ACTIVITY ($\mu\text{Ci}/\text{ml}$)	MEMBRANE DF
6/14/71	0840	1.1×10^{-5}	6.8×10^{-7}	16
	1225	6.3×10^{-5}	4.2×10^{-7}	150
	1530	8.8×10^{-5}	3.2×10^{-7}	280
6/15/71	1030	2.7×10^{-4}	3.1×10^{-6}	87
	1315	1.0×10^{-4}	1.7×10^{-6}	59
	1440	1.3×10^{-4}	1.1×10^{-7}	1200
	1510	1.6×10^{-4}	1.1×10^{-7}	1500
	1530	1.8×10^{-4}	5.7×10^{-7}	320
Average				160

TABLE 2-37
EXPECTED REVERSE OSMOSIS DECONTAMINATION FACTORS
FOR SPECIFIC NUCLIDES (REF. 41)

NUCLIDE	CONCENTRATE ACTIVITY ($\mu\text{Ci}/\text{ml}$)	PRODUCT ACTIVITY ($\mu\text{Ci}/\text{ml}$)	MEMBRANE DF
Co-60	2.5×10^{-4}	5×10^{-7}	500
Mo-99	3.8×10^{-2}	1×10^{-3}	40
I-131, 132, 133, 134, 135	1.2×10^{-1}	4×10^{-3}	30
Cs-134, 137	4.3×10^{-2}	2×10^{-4}	200

unplanned liquid releases. During the period evaluated, 27 unplanned liquid releases occurred, 12 due to personnel error, 7 due to component failures, and the remainder due to miscellaneous causes such as procedural errors and design errors. Table 2-38 summarizes the findings of this evaluation. These findings indicate that approximately 0.15 Ci/yr per reactor is expected to occur as unplanned releases. The tanks most likely to be released are the low-level sample (test) tanks, and therefore the calculated liquid source term radionuclide distribution is applied to the releases.

TABLE 2-38
FREQUENCY AND EXTENT OF UNPLANNED LIQUID RADWASTE
RELEASES FROM OPERATING PLANTS

<u>UNPLANNED LIQUID RELEASES</u>	<u>FREQUENCY/VOLUME</u>
Total number	27
Approximate activity (Ci)	14.0
Approximate volume (gal)	2.0×10^5
Fraction of cumulative occurrence per reactor year (releases/reactor year)	0.3
Activity per release (Ci/release)	0.5
Activity release per reactor year (Ci/reactor year)	0.14
Volume of release per reactor year (gal/reactor year)	2.0×10^3

Operating experience has shown the availability for evaporators in waste treatment systems to be in the range of 60 to 80%. Unavailability is attributed to scaling, fouling of surfaces, instrumentation failures, corrosion, and occasional upsets resulting in high carryovers requiring system cleaning. A value of two consecutive days unavailability per week was chosen as being representative of operating experience. For systems having sufficient tank capacity to collect and hold wastes during the assumed 2-day/week outage, no adjustments are required for the source term. If less capacity is available, the difference between the waste expected during two days of normal operation and the available holdup capacity is assumed to follow an alternative route for processing. Since processing through an alternative route implies mixing of wastes having different purities and different dispositions after treatment, it is assumed that the fraction of waste discharged following processing will be that normally assumed for the less pure of the two waste streams combined.

Since chemical and regenerant wastes are not amenable to processes other than evaporation, it is assumed that unless an alternative evaporation route is available, chemical and regenerant wastes in excess of the storage capacity are discharged without treatment.

2.2.21 GUIDELINES FOR ROUNDING OFF NUMERICAL VALUES

In calculating the estimated annual release of radioactive materials in liquid and gaseous wastes, round off all numerical values to two significant figures.

2.2.22 CARBON-14 RELEASES

2.2.22.1 Parameter

The annual quantity of carbon-14 released from a boiling water reactor is 9.5 Ci/yr. It is assumed that the carbon-14 reacts with oxygen in the reactor water and behaves like a noble gas fission product; thus all carbon-14 produced will be released through the main condenser offgas system.

2.2.22.2 Bases

The principal source of carbon-14 is the thermal neutron reaction with oxygen-17 in the reactor coolant. The production rate of carbon-14 from oxygen-17 is given by the equation:

$$Q = N_{O_{17}} \cdot m \cdot p \cdot s \cdot t \cdot \sigma_0 \cdot \phi \quad (\text{Ci/yr})$$

where

- m is the 3.9×10^4 kg, mass of water in reactor core;
- $N_{O_{17}}$ is the 1.3×10^{22} atoms O-17/kg natural water;
- p is the 0.08, plant capacity factor;
- s is the 1.03×10^{-22} Ci/atom, specific activity for C-14;
- t is the 3.15×10^7 sec/yr, maximum irradiation time per year;
- σ_0 is the 2.4×10^{-25} cm², thermal neutron cross section for O-17; and
- ϕ is the 3×10^{13} neutrons/cm²-sec, average thermal neutron flux.

Based on the above parameters, Q = 9.5 Ci/yr.

Carbon-14 can also be produced by neutron activation of nitrogen-14 dissolved in the reactor coolant and present in air in the drywell. These sources contribute a small fraction of a curie per year to the annual production of carbon-14 due to the low concentration of nitrogen-14 in the reactor coolant (less than 1 ppm by weight), and the low neutron flux in the drywell (approximately 4×10^8 neutrons/cm²-sec).

The annual release of 9.5 Ci of carbon-14 is in good agreement with measurements at Nine Mile Point 1 reported by Kunz et al. (Ref. 42), who found that 8 curies per year of carbon-14 were released, principally in the form of CO₂.

2.2.23 ARGON-41 RELEASES

2.2.23.1 Parameter

The annual quantity of argon-41 released from a boiling water reactor is 25 Ci/yr. The argon-41 is released to the environment via the containment vent when the drywell is vented or purged.

2.2.23.2 Bases

Argon-41 is formed by neutron activation of stable naturally occurring argon-40 in the drywell air surrounding the reactor vessel. The argon-41 is released to the environment when the drywell is vented or purged. BWRs that have a common stack for the release from the main condenser offgas system and the containment purge do not report argon-41 releases because the argon-41 is a small fraction of the total release from the stack. Monticello reported that 50 curies of argon-41 were released in 1973 and that the isotope was not detected in effluents in 1974. Browns Ferry 1 reported 19.2 curies of argon-41 released in 1974. Based on these data, the argon-41 release is estimated to be 25 curies per year.

CHAPTER 3. INPUT FORMAT, SAMPLE PROBLEM, AND
FORTRAN LISTING OF THE BWR-GALE CODE

3.1 INTRODUCTION

This chapter contains additional information for using the BWR-GALE Code. Chapter 1 of this report described the entries required to be entered on input data cards, and Section 3.2 of this chapter contains sample input data sheets to orient the user in making the entries described in Chapter 1.

Section 3.3 of this chapter contains a listing of the input data cards for a sample problem and the resultant output for that sample problem. Section 3.4 contains a discussion of the nuclear data library used and a FORTRAN listing of the BWR-GALE Code.

3.2 INPUT DATA SHEETS

The following pages show (1) the form in which data should be entered on input data sheets and (2) a sample completed sheet.



FORTRAN Coding Form

GX2B-7327-6 U-M 050**
Printed in U.S.A.

PROGRAM Input Data BWR-GALE Code		PROGRAMMING INSTRUCTIONS	GRAPHIC	PUNCH	PAGE 1 OF 2																																																																										
PROGRAMMER		DATE July 1975		CARD PLOTTED NUMBER																																																																											
STATEMENT NUMBER	FORTRAN STATEMENT										COMMUNICATION SEQUENCE																																																																				
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32	33	34	35	36	37	38	39	40	41	42	43	44	45	46	47	48	49	50	51	52	53	54	55	56	57	58	59	60	61	62	63	64	65	66	67	68	69	70	71	72	73	74	75	76	77	78	79
CARD 1	NAME	NAME OF REACTOR []																				TYPE = BWR																																																									
CARD 2	POWTE	THERMAL POWER LEVEL (MEGAWATTS)																				[]																																																									
CARD 3	GTO	TOTAL STEAM FLOW (MILLION LBS/HR)																				[]																																																									
CARD 4	WLIQ	MASS OF WATER IN REACTOR VESSEL (MILLION LBS)																				[]																																																									
CARD 5	GDE	CLEAN-UP DEMINERALIZER FLOW (MILLION LBS/HR)																				[]																																																									
CARD 6	REGENT	CONDENSATE DEMINERALIZER REGENERATION TIME (DAYS)																				[]																																																									
CARD 7	FFCDM	FRACTION FEEDWATER THROUGH CONDENSATE DEMIN																				[]																																																									
CARD 8	DILUT	RADWASTE DILUTION FLOW (THOUSAND GPM)																				[]																																																									
CARD 9	HIGH PURITY WASTE INPUT []										GPD AT []] PCA																																																										
CARD 10	DFI=[]	DFCS=[]	DFO=[]																																																																												
CARD 11	COLLECTION [] DAYS PROCESS []										DAYS FRACT DISCH []																																																																				
CARD 12	LOW PURITY WASTE INPUT []										GPD AT []] PCA																																																										
CARD 13	DFI=[]	DFCS=[]	DFO=[]																																																																												
CARD 14	COLLECTION [] DAYS PROCESS []										DAYS FRACT DISCH []																																																																				
CARD 15	CHEMICAL WASTE INPUT []										GPD AT []] PCA																																																										
CARD 16	DFI=[]	DFCS=[]	DFO=[]																																																																												
CARD 17	COLLECTION [] DAYS PROCESS []										DAYS FRACT DISCH []																																																																				
CARD 18	REGENERANT SOLTNS WASTE INPUT - GPD																																																																														
CARD 19	DFI=[]	DFCS=[]	DFO=[]																																																																												
CARD 20	COLLECTION [] DAYS PROCESS []										DAYS FRACT DISCH []																																																																				
CARD 21	GGS	GLAND SEAL STEAM FLOW (THOUSAND LBS/HR)																				[]																																																									
CARD 22	WSTE	MASS OF STEAM IN REACTOR VESSEL (MILLION LBS)																				[]																																																									
CARD 23	TLM 3	GLAND SEAL HOLD UP TIME (HOURS)																				[]																																																									
CARD 24	TLM 4	AIR EJECTOR OFF GAS HOLDUP TIME (HOURS)																				[]																																																									

*A standard card form, IBM electro 808157, is available for punched statements from this form.

*Number of forms per pad may vary slightly.



FORTRAN Coding Form

GX28-7327-6 U/M 050**
Printed in U.S.A.

STATEMENT NUMBER	ITEM	FORTRAN STATEMENT		IDENTIFICATION SEQUENCE
		1	2	
CARD 25		CONTAINMENT BLDG	CHARCOAL? []	HEPA? []
CARD 26		TURBINE BLDG	CHARCOAL? []	HEPA? [] SPEC FEATURES[]
CARD 27	FIL 3	GLAND SEAL VENT, IODINE PF		[]
CARD 28	FIL 4	AIREJECTOR OFF GAS IODINE PF		[]
CARD 29		AUXILIARY BLDG	CHARCOAL? []	HEPA? []
CARD 30		RADWASTE BLDG	CHARCOAL? []	HEPA? []
CARD 31	KCHAR	CHARCOAL DELAY SYSTEM 0 = 0, 1 = YES, 2 = CRYOGENIC DISTILL		[]
CARD 32	KKR	KRYPTON DYNAMIC ADSORPTION COEFFICIENT (CM ³ /GM)		[]
CARD 33	KXE	XENON DYNAMIC ADSORPTION COEFFICIENT (CM ³ /GM)		[]
CARD 34	KNO	NUMBER OF MAIN CONDENSER SHELLS		[]
CARD 35	KMASS	MASS OF CHARCOAL (THOUSAND LBS)		[]
CARD 36	PFLAUN	DETERGENT WASTE DECON FACTOR		[]

*A standard model from 1987 (electro 580) is also available for permitting. Instruments from Avantech.

^a Number of foams per pad may vary slightly.

3.3 SAMPLE PROBLEM - INPUT AND OUTPUT

The following pages show printouts of the input and output for a sample problem using the BWR-GALE Code.

3
en

CARD 1	NAME	NAME OF REACTOR - SAMPLE KKR CASE	TYPE = SXR
CARD 2	PWTH	THERMAL POWER LEVEL (MEGAHAWTS)	3400.
CARD 3	GTO	TOTAL STEAM FLOW (MILLION LBS/HR)	15.
CARD 4	ALIG	MASS OF WATER IN REACTOR VESSEL (MILLION LBS)	0.38
CARD 5	GDE	CLEANUP DEMINERALIZER FLOW (MILLION LBS/HR)	0.13
CARD 6	REGENT	CONDENSATE DEMINERALIZER REGENERATION TIME (DAYS)	56.
CARD 7	FFCDM	FRACTION FEED WATER THROUGH CONDENSATE DENTN	1.
CARD 8	NILUT	RADIWASTE SITUATION FLOW (THOUSAND GPM)	3.
CARD 9		HIGH PURITY WASTE INPUT 28540. GPD AT .15 PCT	
CARD 10		DFT= 1.0E030FCS= 1.0E020 = 1.0E03	
CARD 11		COLLECTION 1. DAYS PROCESS .07 DAYS FRACT DISCH 0.01	
CARD 12		LOW PURITY WASTE INPUT 5700. GPD AT .13	
CARD 13		DFT= 1.0E030FCS= 1.0E040F0 = 1.0E04	
CARD 14		COLLECTION 3.1 DAYS PROCESS .6 DAYS FRACT DISCH 1.	
CARD 15		CHEMICAL WASTE INPUT 600. GPD AT .02 PCT	
CARD 16		DFT= 1.0E030FCS= 1.0E040F0 = 1.0E04	
CARD 17		COLLECTION 3.1 DAYS PROCESS .6 DAYS FRACT DISCH 1.	
CARD 18		REGENERATION SOLTNS INPUT GPD 1700.	
CARD 19		DFT= 1.0E040FCS= 1.0E050F0 = 1.0E05	
CARD 20		COLLECTION 9.4 DAYS PROCESS .44 DAYS FRACT DISCH 0.1	
CARD 21	GGS	GLAND SEAL STEAM FLOW (THOUSAND LBS/HRT)	0.0
CARD 22	WSTE	MASS OF STEAM IN REACTOR VESSEL (MILLION LBS)	.021
CARD 23	T1M3	GLAND SEAL HOLDUP TIME (HOURS)	
CARD 24	T1M4	AIR EJECTOR OFFGAS HOLDUP TIME (HOURS)	.167
CARD 25		CONTAINMENT BLDG CHARCOAL? YES HEPATEYES	
CARD 26		TURBTNE BLDG CHARCOAL? HEPAT? CLEAN STEAM?YES	
CARD 27	FIL3	GLAND SEAL VENT, TIDINE PF	1.0
CARD 28	FIL4	AIR EJECTOR OFFGAS TOTNE PF	
CARD 29		AUXILIARY BLDG CHARCOAL? HEPAT?	
CARD 30		RADIWASTE BLDG CHARCOAL? HEPAT? HEPATEYES	
CARD 31	KCHAR	CHARCOAL DELAY SYSTEM DEVS,1=YES,2=CRYOGENIC DISTILL	1
CARD 32	KKR	KRYPTON DYNAMIC ABSORPTION COEFFICIENT (CM3/GH)	105.
CARD 33	KXE	XENON DYNAMIC ABSORPTION COEFFICIENT (CM3/GH)	2410.
CARD 34	KNO	NUMBER OF MAIN CONDENSER SHELLS	3.
CARD 35	KMASS	MASS OF CHARCOAL (THOUSAND LBS)	48.
CARD 36	PFLAUN	DETERGENT WASTE DECONTAMINATION FACTOR	1.0

SAMPLE BAR CASE	
THERMAL POWER LEVEL (MEGAWATTS)	1000
PLANT CAPACITY FACTOR	0.80
TOTAL "TEAM" FLOW (MILLION LBS/HR)	100
WATER IN REACTOR VESSEL (MILLION LBS)	40
MASS	
CLEL: *UP DEMINERALIZER FLOW (MILLION LBS/HR)	10
DEMINERALIZER REGENERATION TIME (DAYS)	10
CONDENSATE DEMINERALIZER REGENERATION TIME (DAYS)	10
FEED WATER THROUGH CONDENSADE DEMIN	
FRACTIONATION FLOW (THOUSAND GPH)	100
RADWASTE DILUTION FLOW (THOUSAND GPH)	100

RIGHTS WASTE INPUTS

WASTE INPUTS	FLOW RATE (GAL/DAY)	FRACTION OF PCA DISCHARGED	COLLECTION TIME		DECAY (DAYS)
			TIME (DAYS)	TIME (DAYS)	
URINE	2.85E 04	0.150	0.010	1.000	0.070
URINARY WASTE	5.70E 03	0.130	1.000	3.100	0.600
URINARY WASTE	6.00E 02	0.020	1.000	3.100	0.600
URINAL WASTE	1.70E 03		0.100	9.400	0.440
URINAL SOLS					

GASEOUS WASTE INPUTS
 GLAND SEAL STEAM FLOW (THOUSAND LBS/HR)
 MASS OF STEAM IN REACTOR VESSEL (MILLION LBS)
 GLAND SEAL HOLDUP TIME (HOURS)
 AIR EJECTOR OFFGAS HOLDUP TIME (HOURS)
 CONTAINMENT BLDGDODNE RELEASE FRACTION
 PARTICULATE RELEASE FRACTION
 TURBINE BLDG TDDNF RELEASE FRACTION
 PARTICULATE RELEASE FRACTION
 RELEASE FRACT.=SPECIAL DES. FF
 GLAND SEAL VENT IODINE PF
 AIR EJECTOR OFFGAS IODINE PF
 AUXILIARY BLDG IODINE RELEASE FRACTION
 PARTICULATE RELEASE FRACTION
 RADWASTE BLDG IODINE RELEASE FRACTION
 PARTICULATE RELEASE FRACTION
 THERE IS A CHARCOAL DELAY SYSTEM
 KRYPTON HOLDUP TIME (DAYS)
 XENON HOLDUP TIME (DAYS)
 KRYPTON DYNAMIC ABSORPTION COEFFICIENT (CM³/S)
 XENON DYNAMIC ABSORPTION COEFFICIENT (CM³/S)
 NUMBER OF MAIN CONDENSER SHELLS
 MASS OF CHARCOAL (THOUSAND LBS)

COLLECTION CHARGED	DECAY TIME	DECONTAMINATION TIME	FACTORS
(DAYS)	(DAYS)		OTHERS
0.010	1.000	0.070	1.00E 03
1.000	3.100	0.600	1.00E 03
1.000	3.100	0.600	1.00E 03
0.100	9.400	0.440	1.00E 04

3400	00000	BWR
0	80	*
15	00000	*
0	38000	*
0	13000	*
56	00000	*
1	00000	*
		3.00000

SAMPLE BMR CASE

GASEOUS RELEASE RATE

LEVEL 38394

0.0 APPEARING IN THE TABLE INDICATES RELEASE IS LESS THAN 1.0 CI/YR FOR NOBLE GAS, 0.0001 CI/YR FOR 1

SAMPLE BHR CASE

AIRBORNE PARTICULATE RELEASE RATE

(CURIES PER YEAR)

NUCLIDE	CONTAINMENT BLDG.	TURBINE BLDG.	AUXILIARY BLDG.	RADIWSTE BLDG.	MECH VAC. PUMP	TOTAL
---------	----------------------	------------------	--------------------	-------------------	-------------------	-------

CR=51	3.0E+06	2.6E+03	3.0E+04	9.0E+05	0.0	3.0E+03
HN=54	3.0E+05	1.2E+04	3.0E+03	3.0E+04	0.0	3.4E+03
FE=59	4.0E+06	1.0E+04	4.0E+04	1.5E+04	0.0	6.5E+04
CD=58	6.0E+06	1.2E+04	6.0E+04	4.5E+05	0.0	7.7E+04
CD=60	1.0E+06	4.0E+04	1.0E+02	9.0E+04	0.0	1.1E+02
ZN=65	2.0E+05	4.0E+05	2.0E+03	1.5E+05	0.0	2.1E+03
SR=89	9.0E+07	1.2E+03	9.0E+05	4.5E+06	0.0	1.3E+03
SR=90	5.0E+08	4.0E+06	5.0E+06	3.0E+06	0.0	1.2E+05
3-00	2.0E+06	2.0E+05	4.0E+04	5.0E+07	0.0	4.2E+04
SB=124	2.0E+06	6.0E+05	2.0E+04	5.0E+07	0.0	2.6E+04
CS=134	4.0E+05	6.0E+05	4.0E+03	4.5E+05	3.0E+06	4.1E+03
CS=135	3.0E+06	1.0E+05	3.0E+04	4.5E+06	2.0E+06	3.2E+04
CS=137	5.5E+05	1.2E+04	5.5E+03	9.0E+05	1.0E+05	5.8E+03
BK=140	4.0E+06	2.2E+03	4.0E+04	1.0E+06	1.1E+05	2.6E+03
CE=111	1.0E+06	1.2E+04	1.0E+04	2.6E+05	0.0	2.5E+04

SAMPLE 804R CASE

LIQUID EFFLUENTS

NUCLIDE	HALF-LIFE (DAYS)	CONCENTRATION IN PRIMARY COOLANT (MICRO Ci/ML)	NUCLEAR ACTIVATION PRODUCTS	ANNUAL RELEASES TO DISCHARGE CANAL			ADJUSTED TOTAL DETERGENT WASTES (Ci/YR)	TOTAL (Ci/YR)
				HIGH PURITY (CURIIES)	LOW PURITY (CURIIES)	TOTAL LAS (CURIIES)		
NA 24	6.25E+01	9.00E+03	0.00030	0.00013	0.00000	0.00043	0.000310	0.0
RP 32	1.43E+01	2.00E+04	0.00001	0.00002	0.00000	0.00003	0.00024	0.0
CR 51	2.78E+01	5.00E+03	0.00029	0.00049	0.00017	0.00045	0.00677	0.0
MN 54	3.03E+02	6.00E+05	0.00000	0.00001	0.00000	0.00001	0.00010	0.000110
MN 56	1.07E+01	5.00E+02	0.00029	0.00001	0.00000	0.00030	0.00214	0.000210
FE 55	9.50E+02	1.00E+03	0.00006	0.00010	0.00008	0.00024	0.00170	0.000170
FE 59	4.50E+01	3.00E+05	0.00000	0.00000	0.00000	0.00001	0.00004	0.00004
CO 58	7.13E+01	2.00E+04	0.00001	0.00002	0.00001	0.00004	0.00430	0.00430
CO 60	1.92E+03	4.00E+04	0.00002	0.00004	0.00003	0.00010	0.00068	0.000670
NT 65	1.07E+01	3.00E+04	0.00000	0.00000	0.00000	0.00001	0.00001	0.00001
CU 64	5.33E+01	3.00E+02	0.00091	0.00039	0.00001	0.00126	0.00900	0.000900
ZN 65	2.45E+02	2.00E+04	0.00001	0.00002	0.00001	0.00005	0.00033	0.00033
ZN 69N	5.75E+01	2.00E+03	0.00006	0.00003	0.00000	0.00009	0.00054	0.00054
ZN 69	3.94E+02	0.0	0.00007	0.00003	0.00000	0.00009	0.00068	0.00068
ZR 95	6.50E+01	0.0	0.00010	0.0	0.00000	0.00000	0.00140	0.00140
NB 95	3.50E+01	0.0	0.00010	0.0	0.00000	0.00000	0.00200	0.00200
Y 187	9.96E+01	3.00E+04	0.00001	0.00001	0.00000	0.00002	0.00015	0.00015
NP239	2.35E+00	7.00E+03	0.00039	0.00001	0.00075	0.00000	0.000540	0.0

FISSION PRODUCTS

NUCLIDE	HALF-LIFE (DAYS)	CONCENTRATION IN PRIMARY COOLANT (MICRO Ci/ML)	NUCLEAR ACTIVATION PRODUCTS	ANNUAL RELEASES TO DISCHARGE CANAL			ADJUSTED TOTAL DETERGENT WASTES (Ci/YR)	TOTAL (Ci/YR)
				HIGH PURITY (CURIIES)	LOW PURITY (CURIIES)	TOTAL LAS (CURIIES)		
SR 83	1.00E+01	5.20E+04	0.00001	0.00002	0.00000	0.00002	0.00002	0.000013
SR 89	5.20E+01	4.00E+03	0.00003	0.00001	0.00000	0.00002	0.000015	0.000015
SR 91	4.03E+01	0.0	0.00006	0.00003	0.00000	0.00003	0.000013	0.000013
YY 91H	3.17E+02	0.0	0.00006	0.00002	0.00000	0.00008	0.000058	0.000058
YY 91	5.88E+01	4.00E+05	0.00000	0.00001	0.00000	0.00001	0.000010	0.000009
SR 92	1.13E+01	1.00E+02	0.00006	0.00000	0.00000	0.00006	0.000046	0.000046
YY 92	1.47E+01	6.00E+03	0.00014	0.00014	0.00000	0.00015	0.000111	0.000110
YY 93	4.25E+01	4.00E+03	0.00010	0.00003	0.00000	0.00014	0.000097	0.000097
ZR 95	6.50E+01	7.00E+06	0.00000	0.00000	0.00000	0.00000	0.000001	0.000001
NB 95	3.50E+01	7.00E+06	0.00000	0.00000	0.00000	0.00000	0.000001	0.000001
NB 98	3.54E+02	4.00E+03	0.00000	0.00000	0.00000	0.00000	0.000002	0.000002
MO 99	2.79E+00	2.00E+03	0.00002	0.00012	0.00000	0.00023	0.00164	0.00160
TC 99H	2.50E+01	2.00E+02	0.00040	0.00016	0.00000	0.00056	0.00400	0.00400
RU103	3.96E+01	2.00E+05	0.00000	0.00000	0.00000	0.00000	0.00003	0.000017
RU103H	3.96E+02	0.0	0.00000	0.00000	0.00000	0.00000	0.00003	0.00003
TC104	1.05E+01	2.00E+03	0.00002	0.00000	0.00000	0.00000	0.00001	0.00001
RU105H	5.21E+04	0.0	0.00000	0.00000	0.00000	0.00003	0.00006	0.00006
RU105	1.50E+00	1.00E+04	0.00000	0.00001	0.00000	0.00002	0.000015	0.000015
TE106	3.57E+02	3.00E+06	0.00000	0.00000	0.00000	0.00047	0.00683	0.00240
AG110H	2.53E+02	1.00E+06	0.00000	0.00015	0.00000	0.00017	0.00120	0.00044
TE129H	3.40E+01	4.00E+05	0.00000	0.00078	0.00000	0.0008	0.00560	0.00400
TE129	4.79E+02	0.0	0.00000	0.00006	0.00000	0.00006	0.00042	0.00042
TE131H	1.25E+00	1.00E+04	0.00000	0.00000	0.00000	0.00006	0.00016	0.001300
TE131	8.05E+00	5.00E+03	0.00028	0.00047	0.000139	0.008138	0.00006	0.008100
I132	9.58E+02	3.00E+02	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
I133	8.75E+01	2.00E+02	0.00000	0.00074	0.00000	0.0008	0.03998	0.03998
I134	3.67E+02	7.00E+02	0.00006	0.00000	0.00000	0.00006	0.00042	0.00042
CS134	7.49E+02	3.00E+05	0.00002	0.00000	0.00000	0.00002	0.00016	0.00016
I135	2.79E+01	2.00E+02	0.00037	0.00060	0.00001	0.00038	0.00099	0.00099
CS136	1.30E+01	2.00E+05	0.00001	0.00000	0.00000	0.00001	0.00010	0.00010

SAMPLE 3MR CASF LIQUID EFFLUENTS (CONTINUED)

NUCLEIDE	HALF-LIFE (DAYS)	COOLANT (MICRO CI/ML)	ANNUAL RELEASES TO DISCHARGE CANAL			ADJUSTED DETERGENT WASTES (CI/YR)	TOTAL WASTES (CI/YR)
			IN PRIMARY	HIGH PURITY (CURIES)	LOW PURITY (CURIES)		
CS137	1.10E+04	7.00E+05	0.00004	0.00001	0.00000	0.00005	0.02400
BA137H	1.77E+03	0.0	0.00004	0.00001	0.00000	0.00005	0.00035
CS138	2.24E+02	1.00E+02	0.00002	0.00000	0.00000	0.00002	0.00016
BA139	5.76E+02	1.00E+02	0.00002	0.00000	0.00000	0.00002	0.00015
BA140	1.28E+01	4.00E+04	0.00002	0.00004	0.00001	0.00007	0.00047
LA140	1.67E+00	0.0	0.00000	0.00002	0.00001	0.00003	0.00023
LA141	1.62E+01	0.0	0.00001	0.00000	0.00000	0.00001	0.00006
CE141	3.24E+01	3.00E+05	0.00000	0.00000	0.00000	0.00001	0.00005
LA142	6.39E+02	5.00E+03	0.0001	0.0000	0.0000	0.0001	0.00011
CE143	1.38E+00	3.00E+05	0.00000	0.00000	0.00000	0.00000	0.00002
PRI43	1.37E+01	4.00E+05	0.00000	0.00000	0.00000	0.00001	0.00005
CE144	2.84E+02	3.00E+06	0.00000	0.00000	0.00000	0.00000	0.00520
ALL OTHERS	1.19E+01	0.00001	0.00000	0.00000	0.00001	0.00001	0.00007
TOTAL (EXCEPT TRITIUM)	5.31E+01	0.00534	0.01178	0.00730	0.02441	0.17441	0.24000

TRITIUM RELEASE

42 CURIES PER YEAR

3.4 LISTING OF BWR-GALE CODE

3.4.1 NUCLEAR DATA LIBRARY

Calculation of the releases of radioactive materials in liquid effluents using the GALE Code requires a library of nuclear data available on magnetic tape from the Division of ADP Support, USNRC (301)492-7713. For convenience, the tape consists of five files, written in card image form. The contents of the five files are:

1. File 1: A FORTRAN listing of the liquid effluent code.
2. File 2: Nuclear data library for corrosion and activation products for use with the liquid effluent code.
3. File 3: Nuclear data library for fuel materials and their transmutation products for use with the liquid effluent code.
4. File 4: Nuclear data library for fission products for use with the liquid effluent code.
5. File 5: A FORTRAN listing of the gaseous effluent code.

The tape is written in the following format:

DCB = (RECFM = FB, LRECL = 80, BLKSIZE = 3200)

Use of the tape requires two data cards in addition to those described above containing the plant parameters. For a low enrichment uranium-235 oxide-fueled light water reactor, these cards should always contain the following data:

<u>CARD</u>	<u>COLUMN</u>	<u>INPUT DATA</u>
1	1-72	Title
1	75	The value 2
2	1-10	The value 0.632
2	11-20	The value 0.333
2	21-30	The value 2.0
2	31-40	The value 1.0E-25
2	41-46	The date (month, day, year)
2	48	The value 1
2	50	The value 0
2	52	The value 0

A description of the information contained in the nuclear data library can be found in the report ORNL-4628, "ORIGEN - The ORNL Isotope Generation and Depletion Code," dated May 1973.

3.4.2 FORTRAN PROGRAM LISTING

The remainder of this chapter provides the program listing for the BWR-GALE Code.


```

DATA PGAS$4,5,1,5,15,,7,,33,,UBX4,5,T,5/
DATA YES/!YES/
DATA NTRY,INTER/0,0/,PERH/PARTY,,DI-H/T BARTZ
REAL KKR,XKE,KNU,KHASS
50 FORMAT(20A4)
51 FORMAT(16X,'PLANT CAPACITY FACTOR',T74,F0,B0)
52 FORMAT(52X,B44,12X,A4)
53 FORMAT(16X,1344,A2,F10,5)
54 FORMAT(16X,'PERCENT FUEL WITH CLADDING DEFECTS',T74,F6,5)
55 FORMAT(15X,B44,42,8X,F8,0,7X,F5,3)
56 FORMAT(20X,F8,0,2(5X,F8,0))
57 FORMAT(27X,F8,2,14X,F8,2,18X,F8,2)
58 FORMAT(30X,'FRACTION FRACTION COLLECTION DECAY/TBX,TSTREAM
 1  FLUX RATE OF PCA DISCHARGED TIME TIME1,5X,1 DECONTAMINATI
2 NATION FACTORS/20X,(GAL/DAY)!,23X,(DAYS) (DAYS)!,7X,
3 !!,8X,1CS!,8X,1OTHERS!)
59 FORMAT(2X,444,A2,1PE9,2,1X,4(0FF8,3,2X),3(1PE9,2,1X))
60 FORMAT(79X,I1)
61 FORMAT(16X,'THERE IS A CRYOGENIC DISTILLATION COLUMN/20X,TIODINE
1 AND XENON DECONTAMINATION FACTOR',T70,1'10000,1/20X,TKRYPTON DECONTAMINATI
2 ON FACTOR',T71,1'4000,1/20X,TKRYPTON AND XENON HOLDUP TIME
3 (DAYS)!,T73,1'90,1)
62 FORMAT(16X,'THERE IS NO CHARCOAL DELAY SYSTEM')
63 FORMAT(16X,'THERE IS A CHARCOAL DELAY SYSTEM/20X,TKRYPTON HOLDUP
1 TIME (DAYS)!,T72,F9,5/20X,TXENON HOLDUP TIME (DAYS)!,T72,F9,5/
220X,TKRYPTON DYNAMIC ABSORPTION COEFFICIENT (CM3/GH)!,T72,F9,5/
320X,TXENON DYNAMIC ABSORPTION COEFFICIENT(CM3/GH)!,T71,F10,5/20X,
4 NUMBER OF MAIN CONDENSER SHELLS!,T72,F9,5/20X,TMASS OF CHARCOAL
5 (THOUSAND LBS)!,T72,F9,5)
64 FORMAT(58X,F8,4,35X,I1)
65 FORMAT(16X,'FRACTION IODINE PASSING CONDENSATE DEMINERALIZER',
 1 T71,F10,5)
66 FORMAT(16X,'BLW-DOWN RATE (THOUSAND LBS/HR)!',25X,F8,4)
67 FORMAT(16X,'FLUX RATE THROUGH GAS STRIPPER (GH)!',20X,F8,4)
68 FORMAT(70X,F10,5)
69 FORMAT(2X,1BLWDOWN,10X,1PE9,2,14X,0FF5,3,2X,2(F8,3,2X),
 13(1PE9,2,1X))
70 FORMAT(2X,'UNTREATED BLW-DOWN!',1PE9,2,11X,1 1.000 0.0
 10.0 1.00E 00 1.00E 00)
71 FORMAT(2X,'REGENERANT BLSB',1PE9,2,14X,0FF5,3,2X,2(F8,3,2X),
 13(1PE9,2,1X))
72 FORMAT(16X,'PRIMARY COOLANT LEAK TO AUXILIARY BLDG (LB/DAY)!',T72,
 1'160,1)
73 FORMAT(16X,'FREQUENCY OF PRIMARY COOLANT DEGASSING (TIMES/YR)!',T74,0001130
 1,12,1/16X,'PRIMARY TO SECONDARY LEAK RATE (LB/DAY)!',T72,F10,1)
74 FORMAT(16X,'THERE IS A KIDNEY FILTER/20X,TCONTAINMENT ATMOSPHERE 00001050
1CLEANUP RATE (THOUSAND CF)!',T71,F10,5/20X,TPURGE TIME OF CONTAINMENT
2ENT (HOURS)!,T71,F10,5)
75 FORMAT(16X,'THERE IS NOT A KIDNEY FILTER')
76 FORMAT(16X,'THERE IS NOT A CONDENSATE DEMINERALIZER')
77 FORMAT(16X,'FRACTION IODINE BYPASSING CONDENSATE DEMINERALIZER',
 17X,T72,F9,5)
900 FORMAT(16X,'IODINE PARTITION FACTOR (GAS/LIQUID) IN STEAM GENERATOR
 1R ',F4,2)
901 FORMAT(16X,'THERE IS A CRYOGENIC OFFGAS SYSTEM/20X,TIODINE AND XE
1ION DECONTAMINATION FACTOR',T70,1'10000,1/20X,TKRYPTON DECONTAMINATI
2ON FACTOR!,T71,1'4000,1)
902 FORMAT(16X,'THERE IS NOT A CRYOGENIC OFFGAS SYSTEM')
903 FORMAT(16X,1BA44)
904 FORMAT(//,' LIQUID WASTE INPUTS')
905 FORMAT(//,' GASEOUS WASTE INPUTS')

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READ(50,56)DFIUA,DFCSU+,DFU+	00001820
READ(50,57)TU,TSTURD,DFRD	00001830
WRITE(51,58)HARD,DFRLH,TA,DFRDL,TU,TSTURD,DFRDL+,DFCSU+,DFU+	00001840
READ(50,59)HARD,DFRLH,CHAFR,CHA	00001850
READ(50,59)DFCTM,DFESCH,DFLH	00001860
READ(50,57)TDM,TSTURB,DFRD	00001870
WRITE(51,59)HARD,CHAFR,CHA,DFRLH,TDM,TSTURB,DFRDL,DFCSU+,DFU+	00001880
READ(50,60)RG+FH	00001890
READ(50,58)DFIRG,DFLSHG,DFRH	00001900
READ(50,57)TRG,TSTURR,DFRH	00001910
WRITE(51,71)RG+FH,DFGPO,TRG,TSTURR,DFLHG,DFLSHG,DFRH	00001920
READ DATA FOR BAR GAS CODE	00001930
WRITE(51,915)	00001940
READ(50,53)HHD,GGS	00001950
WRITE(51,53)HHD,GGS	00001960
READ(50,53)HHD,ESTE	00001970
WRITE(51,53)HHD,ESTE	00001980
READ(50,53)HHD,TIM3	00001990
WRITE(51,53)HHD,TIM3	00002000
READ(50,53)HHD,TIM4	00002010
WRITE(51,53)HHD,TIM4	00002020
HEPA1#1.0	00002030
FIL1#1.0	00002040
HEPA2#1.0	00002050
FIL2#1.0	00002060
HEPA5#1.0	00002070
FIL5#1.0	00002080
HEPA8#1.0	00002090
FIL8#1.0	00002100
CSRF#1.0	00002110
READ(50,925)HHD,CBCH,CHHEPA	00002120
IF(CBCH,EQ,YES)FIL1#0.1	00002130
IF(CBHEPA,EQ,YES)HEPA1#0.01	00002140
WRITE(51,926)=HHD,FIL1,HEPA1	00002150
READ(50,927)HHD,TBCH,TBHEPA,TBCS	00002160
IF(TBCH,EQ,YES)FIL2#0.1	00002170
IF(TBHEPA,EQ,YES)HEPA2#0.01	00002180
IF(TBCS,EQ,YES)CSRF#0.2	00002190
WRITE(51,928)=HHD,FIL2,HEPA2,CSRF	00002200
READ(50,53)HHD,FTL3	00002210
WRITE(51,53)=HHD,FIL3	00002220
READ(50,53)HHD,FTL4	00002230
WRITE(51,53)=HHD,FIL4	00002240
READ(50,925)=HHD,AXCH,AXHEPA	00002250
IF(AXCH,EQ,YES)FIL5#0.1	00002260
IF(AXHEPA,EQ,YES)HEPA5#0.01	00002270
WRITE(51,926)=HHD,FIL5,HEPA5	00002280
READ(50,925)=HHD,RACH,RAHEPA	00002290
IF(RACH,EQ,YES)FIL6#0.1	00002300
IF(RAHEPA,EQ,YES)HEPA6#0.01	00002310
WRITE(51,926)=HHD,FIL6,HEPA6	00002320
READ(50,60)KCHAR	00002330
READ(50,53)=HHD,KRN	00002340
READ(50,53)=HHD,KRE	00002350
READ(50,53)=HHD,KRU	00002360
READ(50,53)=HHD,KMASS	00002370
IF(KCHAR,EQ,0) GO TO 90	00002380
IF(KCHAR,EQ,1) GO TO 91	00002390
WRITE(51,61)	00002400

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      CHTI1=90,
      CHTI2=90,
      GO TO 92
90  WRITE(S1,B2)
      CHTI1=0,
      CHTI2=0,
      GO TO 92
91  F=10.*KNU
      CHTI1=(0.53*KMASS*KKH)/(F*24.*Z.)
      CHTI2=(0.53*KMASS*KKE)/(F*24.*Z.)
      WRITE(S1,B3)CHTI1,CHTI2,KKH,KKE,KNU,KMASS
92  CONTINUE
      CON=0.,UD
      P3=0.,01
      READ(S0,S3)  NURD,PFLAUN
      IF(PFLAUN.LE.0.0)  WRITE(S1,907)
C      CONVERSION OF UNITS
C
      GTU=GTU*1000000.
      GDE=GDE*1000000.
      GGS=GGS*1000.
      KLIN=LIN*1000000.
      KSTER=STER*1000000.
      WRITE(S1,908)
      WRITE(S1,903)NAHE
      WRITE(S1,214)
214  FORMAT(1HU,131H*****)
      1*****                                         00002700
      2*****                                         00002710
      WRITE(S1,235)                                         00002730
235  FORMAT(1HU,8X,TGASEOUS RELEASE RATE/T1H,Y3X,F10.4)EQUITIES PER YEAR)T20002740
      11H9,16X,1CONSTANT CONC.,1,3X,1CONTAINMENT,5X,1TURBINE,4X,1AUXILIARY00002750
      2Y1,3X,1RADASTET,5X,1GLAND,1,7X,1AIRT,6X,1ECH VACT/1H,4X,1NUCLIDE00002760
      3X3X,1(MICROCURIES/GJ),6X,1BLDG,1,7X,1BLDG,1,7X,1BLDG,1,7X,1BLDG,1,00002770
      4BX,1SFAL,5X,1EJECTURE,2X,1PUNCT,11X,1TOTAL)
      WRITE(S1,214)                                         00002780
      TRITH IS THE BH TRITIUM EOLIANT CONCENTRATION IN UCI/GM 00002790
      TRITPH=.005*P00TH
      TRITCO=.01
      TLH=1.32*(C4R0*CAFLR+0.5*FLH*CHFO*(CMAFH*1800.))
      TRITH=TRITCO*TLH
      IF(TRITH.GT.0.5*TRITPH)TRITHL=0.5*TRITPH 00002830
      TRITHG=TRITPH*TRITHL
      DIV=10.,**INT(CALUG10(TRITHG))+1 00002840
      DIV1000
      ITRITG=INT(TRITHG/DIV+0.5)*10IV
      IIT=1 00002850
      IF(ABS(P0XTH*34000),GT,400,10) GO TO 210 00002860
      IF(Abs(XLIG=3,SE5),GT,0,40015)GO TO 210 00002870
      IF(Abs(GDE=1,3E5),GT,0,20015)GO TO 210 00002880
      IF(Abs(GTU=1,5E7),GT,0,20015)GO TO 210 00002890
      IF(Abs(FFCD=0,9),GT,0,10011)GO TO 210 00002900
      GO TO 211 00002910
210  RHAL2=(GDE*0.9*FFCD*GT0*0.018)/XLIG 00002920
      137#2 00002930
211  CONTINUE
      DISI#1,15 00002940
      DECDH(1)=DECDC(1)*3600. 00002950
      EX3(I)=DECDC(I)*T1H3 00002960
      IF(EX3(I),GT,.75,)EX3(I)=.75, 00002970

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EX4(I)=DEC0H(I)*TINA
 IF(EX4(I),GT,75.)EX4(I)=75.
 IF(I,GT,13)GO TO 2000
 X(I)=XH(I)
 CBL(I)=CBL(I)
 AXBL(I)=AXBL(I)
 TBL(I)=TBL(I)*CSRF
 RAUBL(I)=RAUBL(I)
 SGL(I)=GGG*X1(I)*EXP(-EX3(I))*3.977*UPRFA
 EXC(I)=DEC0H(I)*CHT11*24.
 IF(I,GT,6)EXC(I)=DEC0H(I)*CHT12*24.
 IF(EXC(I),GT,75.)EXC(I)=75.
 UFCRE=0.
 IF(KCHAR,EG,2) UFCR=0.00025
 IF(KCHAR,EG,2,AND,I,GT,8) UFCR=0.0001
 EJT(I)=GTU*X1(I)*EXP(-EX4(I))*(UFCR+EXP(-EXC(I)))*3.977*UPRFA
 GO TO 2001
 2000 CONTINUE
 IF(IDT,EW,1)GO TO 2002
 XH(I)=XH(I)*(111.76*P0*ATHAL1Q)*(1.018*DEC0H(I))/XHAL2 + DEC0H(I)
 2002 X1(I)=XH(I)*CIN
 CBL(I)=CBL(I)*FILE
 AXBL(I)=AXBL(I)*FILE
 TBL(I)=TBL(I)*FILE*CSRF
 RAUBL(I)=RAUBL(I)*FILE
 SGL(I)=GGG*X1(I)*P3*FILE3*EXP(-EX3(I))*3.977*UPRFA
 EXC(I)=0.
 IF(KCHAR,EG,2)EXC(I)=DEC0H(I)*CHT11*24.
 IF(EXC(I),GT,75.)EXC(I)=75.
 IF(KCHAR,EG,2) UFCR=0.00010
 EJT(I)=5.0*EXP(-EX4(I))*(UFCR+EXP(-EXC(I)))*FILE4
 IF(I,EW,15) EJT(15)=EJT(15)*XB(15)/XB(14)
 2001 TEST#1.
 IF(I,GT,13) TEST#0.0001
 IF(SGL(I),LE,TEST1) SGL(I)=0.0
 IF(EJT(I),LE,TEST1) EJT(I)=0.0
 5 CONTINUE
 MSIG#1
 NSIG#15
 CALL SIGF2(TBL)
 CALL SIGF2(SGL)
 CALL SIGF2(EJT)
 DO 2003 I#1,15
 TOT(I)=AXBL(I)+TBL(I)+SGL(I)+EJT(I)+CBL(I)+RAUBL(I)+VPRH(I)
 2003 CONTINUE
 CALL SIGF2(TUT)
 GASTOT#0.
 DO 2004 I#1,13
 WRITE(51,230)EUCLID(I),XB(I),CBL(I),TBL(I),AXBL(I),RAUBL(I),
 1 SGL(I),EJT(I),VPRH(I),TOT(I)
 GASTOT=GASTOT+TOT(I)
 2004 CONTINUE
 230 FORMAT(1H0,4X,A8,5X,1PE9.3,BX,1PE7.1,1X,E4X,1PE7.1,1X),7X,1PE7.1)00003580
 DIV#10,**(INT(ALUG10(GASTOT))#1)
 GASTOT#AINT(GASTOT/DIV+0.5)*DIV
 WRITE(51,232) GASTOT
 232 FORMAT(1H0,5X,'TOTAL NOBLE GASES!', 99X,1PE7.1)
 DO 2008 I#14,15
 WRITE(51,230)EUCLID(I),XB(I),CBL(I),TBL(I),AXBL(I),RAUBL(I),
 1 SGL(I),EJT(I),VPRH(I),TOT(I)
 2008 CONTINUE
 00003640

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      WRITE(51,215) 1TRITG          00003650
215 FORMAT(1H0,5X,'TRITIUM GASEOUS RELEASES',12X,14X,' Curies/yr') 00003660
      WRITE(51,214)          00003670
      WRITE(51,251)          00003680
231 FORMAT(1H0,10X APPEARING IN THE TABLE INDICATES RELEASE IS LESS 00003690
1 THAN 1.0 Ci/yr FOR MOBILE GAS, 0.0001 Ci/yr FOR LT) 00003700
      b CONTINUE          00003710
      WRITE (51,906)          00003720
      WRITE (51,903)NAKE          00003730
      WRITE (51,214)          00003740
      WRITE (51,245)          00003750
245 FORMAT (1H0,49X,TAIRBORN PARTICULATE RELEASE RATE),1H0,65X,1(CUR100003760
1ES PER YEAR),1H0,38X,1CONTAINMENT,3X,TURBINE,8X,TAUXILIARY,4X00003770
2,TAUXAESTE,TECH VAC,1H4,4X,NUCLIDES,24X,THLUG,17X,THLUG,17X,00003780
3THLUG,17X,THLUG,17X,THLUG,17X,THLUG,17X,1TOTAL,0 00003790
      WRITE (51,214)          00003800
      DO 250 I=1,15          01003810
      PCBL(I)=PCBH(I)/1E3*HEPA1          00003820
      PTBL(I)=PTBH(I)/1E3*HEPA2*LSRF          00003830
      PVPL(I)=PVPH(I)/1E3          00003840
      PAXBL(I)=PAXBH(I)/1E3*HEPA5          00003850
      PRXBL(I)=PRXBH(I)/1E3*HEPA6          00003860
      PTUTBL(I)=PCBL(I)+PTBL(I)+PAXBL(I)+PRXBL(I)+PVPL(I)          00003870
      250 CONTINUE          00003880
      NSIG#2          00003890
      NSIG#15          00003900
      CALL SIGF2(PTUTB)          00003910
      DO 253 I=1,15          00003920
      WRITE (51,920) SPART(I),PCBL(I),PTBL(I),PAXBL(I),PRXBL(I),PVPL(I),00003930
      1PTUTB(I)
253 CONTINUE          00003940
      WRITE (51,214)          00003950
      GI TO 80          00003960
      80003970
      80003980
      80003990
      80004000
      C THIS SECTION TREATS PAR RELEASES
      C
1003 READ(50,53)URDU,PRUTH          00004010
      WRITE(51,53)URDU,PRUTH          00004020
      UPFRAM=0,B0          00004030
      WRITE(51,51)          00004040
      READ(50,53)URDU,PRIVOL          00004050
      WRITE(51,53)URDU,PRIVOL          00004060
      600 PER#0,12          00004070
      WRITE(51,54)PER          00004080
      READ(50,53)URDU,DEH1FL          00004090
      WRITE(51,53)URDU,DEH1FL          00004100
      READ(50,53)URDU,CRLR          00004110
      WRITE(51,53)URDU,CRLR          00004120
      READ(50,53)URDU,GEN          00004130
      WRITE(51,53)URDU,GEN          00004140
      READ(50,53)URDU,TOSTFL          00004150
      WRITE(51,53)URDU,TOSTFL          00004160
      READ(50,53)URDU,ST          00004170
      WRITE(51,53)URDU,ST          00004180
      READ(50,53)URDU,LI          00004190
      WRITE(51,53)URDU,LI          00004200
      WL1#GEN#LI          00004210
      READ(50,53)URDU,TMSC          00004220
      WRITE(51,53)URDU,TMSC          00004230
      READ(50,60)TBU,XFRNT          00004240
      WRITE(51,60)TBU          00004250

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IF(KFNRIT,ER,0) GO TO 801
KFRTSC#0,9
WRITE(51,910)
GO TO 802
801 WRITE(51,911)
FVRTSC#1,0
802 CONTINUE
READ(50,53)HARD,REGENT
WRITE(51,53)HARD,REGENT
C READ DATA FOR PAR LIQUID CODE
C
READ(50,53)HARD,PFCDM
WRITE(51,53)HARD,PFCDM
READ(50,53)HARD,DILUT
WRITE(51,53)HARD,DILUT
READ(50,912)HARD,SLDR
CXA#1,0
READ(50,56)UFID#,DFCSCH,UFCD
READ(50,57)TC,TSTORE,CAPD
WRITE(51,58)
WRITE(51,59)HARD,SLDR,DXA,DFU,TC,TSTORE,DFID#,DFCSU,UFCD
READ(50,55)HARD,EDFLR,EDA
READ(50,56)UFID#,DFCSU,UFCD
READ(50,57)TE,TS,EDFD
WRITE(51,59)HARD,EDFLR,EDA,EDFU,TE,TS,UFID#,DFCSU,UFCD
READ(50,55)HARD,DFL2,DXA
READ(50,56)UFID#,DFCSU,DFUW
READ(50,57)TD,TSTORE,DAFD
WRITE(51,59)HARD,DFL2,DXA,UFID#,TSTORE,DFID#,DFCSU,UFCD
READ(50,55)HARD,DFL2,DXA
READ(50,56)UFID#,DFLSN2,UFCD
READ(50,57)T2,TSTORE,DXF2
WRITE(51,59)HARD,DFL2,DXF2,UFID#,T2,TSTORE,DFID#,DFCSU,UFCD
READ(50,58)HARD,DFL2,DXF2,UFID#,T2,TSTORE,DFID#,DFCSU,UFCD
READ(50,56)UFID#,DFCSCH,UFCD
READ(50,57)TC,TSTORE,DFCD
READ(50,58)RGXFR
READ(50,56)UFID#,DFCSH,GFRG
READ(50,57)THG,TSTORE,HGF
IF(THD,EN,0,0) GO TO 800
BDFR#TBK#1,UE3*BDFR#0,3476
WRITE(51,69)BDFR,HGF,TCM,TSTORE,UFID#,DFCSCH,UFCD
BDFR#TBK#1,UE3*BHS#1,BDFR#0,3476
WRITE(51,70)BDFR
IF(FFCDM,EN,0,0)GO TO 801
800 CONTINUE
IF(REGENT,ER,0,0) GO TO 802
WRITE(51,71)RGXFR,RGFR,THG,TSTORE,DFING,DFCSHG,DFRG
GO TO 801
802 RGFR#0,0
WRITE(51,71)RGXFR,RGFR,THG,TSTORE,DFING,DFCSHG,DFRG
801 CONTINUE
C READ DATA FOR PAR GAS CODE
C
WRITE(51,905)
READ(50,60)KGTRAT
IF(KGTRAT,EN,0,0) GO TO 8801
GTR#=(DEMFL=SLDR/1440,1/EN1FL

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IF(KGTHHT,EU,2) GO TO 8803          60004870
WRITE(51,909)                         60004880
GO TO 8802                           60004890
8803 GTH=0,25*GTH                   60004900
WRITE(51,940)                         60004910
GO TO 8802                           60004920
8801 GTH=0,0                         60004930
WRITE(51,908)                         60004940
8802 8R8#GTH#UEH!FL+(SHLD#*EDFLH)/1440, 60004950
      WRITE(51,873)SHR
      READ(50,53)HURU,TAU1
      WRITE(51,53)HURU,TAU1
      READ(50,53)HURU,TAU2
      WRITE(51,53)HURU,TAU2
      READ(50,53)HURU,TAU3
      WRITE(51,53)HURU,TAU3
      AXLR#16U
      WRITE(51,72)
      PCLPF#0,0075
      WRITE(51,931)PCLPF
      GHHEPA#1,0
      FRIAH#1,0
      AXHEPA#1,0
      FPPF#1,0
      CSHEPA#1,0
      FRPPV#1,0
      CNHEPA#1,0
      READ(50,932)HURU,GHT
      IF(GAHT,EU,YES)GHHEPA#0,01
      WRITE(51,933)HURU,GHHEPA
      READ(50,934)HAKU,AXCH,AXHT
      IF(AXCH,EU,YES)FRIAH#0,1
      IF(AXHT,EU,YES)AXHEPA#0,01
      WRITE(51,935)HAKU,FRIAH,AXHEPA
      FAUX#PCLPF#FRIAH
      READ(50,53)HURU,CONVOL
      WRITE(51,53)HURU,CONVOL
      EM#2,0
      GENL#100,
      CLNG#0,01
      CLFI#0,00001
      WRITE(51,73)
      READ(50,53)HURU,CFM
      PURTIN#16
      IF(CFM,EU,0,0)GO TO 803
      KID#1
      WRITE(51,74)CFM,PURTIN
      GO TO 804
803 KID#0
      WRITE(51,75)
804 CONTINUE
      IF(FFCDH,GT,0,0)GO TO 805
      WRITE(51,76)
      GO TO 806
805 FIBCD#1,0=FFCD#
      WRITE(51,77)FIBCD
806 CONTINUE
      IF(TBU,EU,0,0)GO TO 809
      CON#0,01
      WRITE(51,900)CON
      GO TO 810

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809 CON=1.0          00005480
      WRITE(51,900)CON          00005490
810 CONTINUE          00005500
      READ(50,936)WARD,CSCH,CSHT,ENPU          00005510
      IF(CSCH,EQ,YES)FPFP#0.1          00005520
      IF(CSHT,EQ,YES)CSHEPA#0.01          00005530
      ENPU#0+ENPU          00005540
      WRITE(51,937)EN          00005550
      WRITE(51,435)WARD,FPFP,CSHEPA          00005560
      FPFP#FPFP          00005570
      READ(50,913)WARD,PNOV1,CNCH,CNHT          00005580
      IF(CNCH,EQ,YES)FPFP#0.1          00005590
      IF(CNHT,EQ,YES)CNHEPA#0.01          00005600
      IF(PNOV1,LT,1.0) GO TO 8811          00005610
      WRITE(51,914)WARD,PNOV1,WARD,FPFP#,CNHEPA          00005620
      GO TU 8812          00005630
8811 WRITE(51,938)          00005640
8812 CONTINUE          00005650
      FPFP#FPFP#          00005660
      TBLK#1700          00005670
      WRITE(51,930)TBLK          00005680
      READ(50,53)WORD,FVN          00005690
      WRITE(51,53)WORD,FVN          00005700
      READ(50,53)WORD,FEJP          00005710
      WRITE(51,53)WORD,FEJP          00005720
      FEJP#FEJP#0.15          00005730
      KCRYU#0.0          00005740
      IF(KCRYU,EQ,0.0) GO TO 811          00005750
      WRITE(51,901)          00005760
      GO TU 812          00005770
3-21   811 WRITE(51,902)          00005780
812 CONTINUE          00005790
      READ(50,53) WORD,PFLAUN          00005800
      IF(PFLAUN,LE,0.0) WRITE(51,907)          00005810
      C
      C           CONVERSION OF UNITS
      C
      TUSTFL=TUSTFL*1000000.          00005820
      *ST=*ST*1000.          00005830
      *LI=*LI*1000.          00005840
      CONVOL=CONVOL*1000000.          00005850
      CFM=CFM*1000.          00005860
      THRTHD#1E3          00005870
      PRIVOL=PRIVOL*1E3          00005880
      DEMIFL=DEMIFL*500.53          00005890
      SHDR#SHDR*,3476          00005900
      EDFLR#EDFLR*,3476          00005910
      DFLR#DFLR*,3476          00005920
      DFL2#DFL2*,3476          00005930
      CBLR#CBLR*500.53          00005940
      H3PRP#H3PRP*.4#POTH          00005950
      H3CUPA IS THE PAR TRITIUM PRIMARY COOLANT CONCENTRATION IN UCI/GH 00005960
      H3CUPA#1.0          00005970
      TPLRP#SHDR#CWA#CWFU+EDFLR#EDAK#DFU+DFLR#DWA#DFU+DFL2#U+2#DF2#0#6#0#1#0          00005980
      H3RLP#TPLRP#H3CUPA#3.977          00005990
      IF(H3RLP#,GT,0.5*H3PRP#)-H3LP#=0.5*H3PRP#          00006000
      H3RLG#H3PRP#=H3RLP#          00006010
      DIV#10.*#(INT(ALUG10(H3RLG)))-1          00006020
      IDIV#DIV          00006030
      IHLRG#INT(H3RLG/DI#>0.5)*IDIV          00006040
      IF(TAU3,EQ,0.)TAU3#0.1          00006050

```

SRB#SRB#500,55
 PE#565,TAU3
 T1#3,1557E7/ENCLPRA
 T3#3,1557E+07/PE
 T4#TAU1#86400,
 T5#TAU2#86400,
 DO 845 I=1,15
 845 DEC(HI)*DEC(1)*3600,
 DO 850 I=1,15
 850 CONCP(I)=XPICTD
 IF(ABS(PRAUTH=5400),GT,400,1260) TU 855
 IF(ABS(PRIVL=5,SE5),GT,,S001E5) GU TU 855
 IF(ABS(CLFL=5,7E4),GT,,S001E4) GU TU 855
 IF(ABS(SBLDR=625,),GT,375,.1) GU TU 855
 IF(ABS(CHFLR=5750,),GT,3750,.1) GU TU 855
 IF(KGTR=T,GT,0) GU TU 855
 GO TU 861
 855 AFPTEG#1,0
 RNG2=(SBLDR+DEFL*GT)-XPIVOL
 RHAL2=(DEFL*GT+900,1*SBLDR)/XPIVOL
 RX2G#161,76*PRATH/XPIVOL
 DO 860 I=1,15
 IF(I,GT,13) GU TU 858
 CONCP(I)=CONCP(1)*RX2G*(,00091*DEC(HI))/RNG2*DEC(HI)
 GU TU 860
 858 CONCP(1)=CONCP(1)*RX2G*(,00091*DEC(HI))/RHAL2*DEC(HI)
 860 CONTINUE
 861 CONTINUE
 IF(TBU,EG,0,0)GU TU 880
 IF(FFCOM,LE,0,01)GU TU 870
 P+TYPE#1,0
 DO 865 I=1,15
 865 CONCS(I)=XP2(I)
 CONCS(14)#6,8E+6
 CONCS(15)#6,4E+6
 RSTAN#_5E17
 IF(AFPTEG,EG,1,0) GU TU 890
 IF(ABS(ALI=4,5E5),GT,,S001E5) GU TU 890
 IF(ABS(TUSTFL=1,5E7),GT,,2001E7) GU TU 890
 IF(ABS(THU=7,5E4),GT,2,S001E4) GU TU 890
 IF(ABS(FFCOM=.65),GT,,1001) GU TU 890
 GO TU 896
 870 P+TYPE#2,0
 DO 875 I=1,13
 875 CONCS(I)=XP2(I)
 CONCS(14)#1,1E+4
 CONCS(15)#6,5E+5
 RSTAN#_02
 IF(AFPTEG,EG,1,0) GU TU 890
 IF(ABS(ALI=4,5E5),GT,,S001E5) GU TU 890
 IF(ABS(TUSTFL=1,5E7),GT,,2001E7) GU TU 890
 IF(ABS(THU=7,5E3),GT,1,S001E3) GU TU 890
 IF(ABS(FFCOM=.005),GT,,.005001) GU TU 890
 GU TU 896
 880 P+TYPE#3,0
 DO 885 I=1,13
 885 CONCS(I)=XP2(I)
 CONCS(14)#1,3E+7
 CONCS(15)#1,8E+7
 IF(AFPTEG,EG,1,0)GU TU 890
 IF(ABS(TUSTFL=1,5E7),GT,,2001E7) GU TU 890

```

1F(ABS(FFCDH=.65.,GT.,10012 GO TO 890
GO TO 898
890 RHAL3#(160*FHRSCH,9*CLK*TUSTFL*FFCDH)/XLI
DO M95 I#1,15
IF(I,GT,13)GO TO 892
CONCS(I)=CONCS(I)*1.5E7/TUSTFL*(CNC(I)/XP1(I))
GO TO 895
892 KATH#3,7
IF(PATYPE,EN,3,0)GO TO 893
CONCS(I)=CONCS(I)*(4.5E5/LI)*(HSTAN+DECOSH(I))/((RHAL3+DECOSH(I))*CNC(I)/XP1(I))
GO TO 895
893 CONCS(I)=CONCS(I)*(6.77E6/(LI*RHAL3))*(CNC(I)/XP1(I))
895 CONTINUE
896 PNUV=PNUV1/CURVUL*60.
C THIS PART OF PROGRAM IS FOR KLELÉ GASES
CRYD#0,0
D07I#1,15
X2(I)=(DECOUN(I)+PNUV/3600.*I)*T1
IF(X2(I),GT,75.) X2(I)=75.
X3(I)=DECOUN(I)*T5
IF(X3(I),GT,75.) X3(I)=75.
X4(I)=DECOSH(I)*T4
IF(X4(I),GT,75.) X4(I)=75.
X5(I)=DECOSH(I)*T5
XDK#X5(I)
IF(X5(I),GT,75.) X5(I)=75.
XCRYD#DECOUN(I)*800
IF(XCRYD,GT,75.) XCRYD=75.
IF(I,GT,13)GO TO 1030
IF(I,GT,5) XDK#X4(I)
IF(KCHYD,EN,1) CRYD#2,5E-4
IF(I,GT,5,AND,XCHYD,EN,1) CRYD#1,0E-4
CTPHO(I)=(CNC(I)*PRIVOL*CLHNG)/(DECOSH(I)+PNUV)*1.892E-5
ACUNT(I)=CTPHO(I)*(1,-EXP(-X2(I)))
ASHIMC(I)=(CONCH(I)*SRB)/DECOSH(I)*4.54E-4*(1,-EXP(-X3(I)))
AXBL(I)=CUNCP(I)*AUXLR*.1657*OPRKA
CBCP(I)= EN * PNUV * (CTPHO(I)*T1/3600.+CTPHO(I)*(EXP(-X2(I))+1.))00007120
1/(DECOSH(I)+PNUV)
CHSP(I)=EN*ACUNT(I)
CBL(I)=CHCP(I)+CHSP(I)
ASHIMC(I)=PE*ASHM(I)*(EXP(-XDK)+CHYD*EXP(-XCRYD))*OPRKA
ASHIMB(I)=EM*CBCP(I)*PRIVOL*.54E-4*(EXP(-XDK)+CRYD*EXP(-XCRYD)) 00007170
EJT(I)=CONCS(I)*TUSTFL*3.977*OPRKA
THL(I)=CONCS(I)*THLK*3.977*OPRKA
BVUG(I)=0.0
TEST#1,0
IF(CBL(I),LT,TEST)CBL(I)=0.0
IF(ASHIM(S(I),LT,TEST)ASHIM(S(I))=0.0
IF(ASHIMC(I),LT,TEST)ASHIMC(I)=0.0
IF(EJT(I),LT,TEST)EJT(I)=0.0
IF(TBL(I),LT,TEST)TBL(I)=0.0
IF(AXBL(I),LT,TEST)AXBL(I)=0.0
GO TO 1031
C THIS PART OF PROGRAM IS FOR IODINE

```

C

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1030 CTPROC(1)*(CONCP(1)*PRIVILE*CLF1)*LDECOR(1)*PNOV*1,892E+5      00007310
ACUNT(I)*CTPHU(1)*1,-EXP(-X2(1))           00007320
AXBL(I)*CUNCR(1)*AUXLR*,1657*(PFH3*FAUX  00007330
ASHIMC(I)=0,0                                00007340
ASHIMS(I)=0,0                                00007350
CHCP(1)= EN * PNOV * (CTPHU(1)*1/3600.+CTPROC(1)*(EXP(-X2(1))+1,00007360
1/(DECOR(1)+PNOV))*PFH3                    00007360
CHSP(1)=EN*ACUNT(I)*PFH3                   00007390
CHL(I)=CBCP(1)+CBSP(1)                      00007400
FVI=0,05                                     00007410
EJT(I)=CUNCR(I)*GENL*FVI*FELJ*,1657*PFH3
TBL(I)=CUNCS(I)*CUN*THLK*3,977*PFH3       00007420
BVUG(I)=CUNCS(I)*TBG*FV*,3,977*PFH3        00007430
IF(KIN,ER,0) GL TO 4002                     00007440
DLAK=((CFM*57./CONVL)+DECOR(I))            00007450
EXX2=DLAK*PURTIN                           00007460
IF(EXX2.GT.75,)EXX2=75,                      00007470
EXPF=EXP(-EXX2)                             00007480
EXPC=1,-EXPF                               00007500
ELSS=PFH*CHNL(1)*PRIVILE*CLF1*1,892E+5*DLAK*EXPC
CHL(I)=CHSP(I)*EXPF+ELSS*EN+CHCP(1)*(1,-PI*HTH/(8760.*PFH3/EN)) 00007510
4002 TEST#0,001                               00007520
IF(CBL(I),LT,TEST)CHL(I)=0,0                00007530
IF(EJT(I),LT,TEST)EJT(I)=0,0                00007540
IF(BVUG(I),LT,TEST)BVUG(I)=0,0              00007550
IF(TBL(I),LT,TEST)TBL(I)=0,0                00007560
IF(AXBL(I),LT,TEST)AXBL(I)=0,0              00007570
00007580
C 1031 CONTINUE                               00007590
C 7 CONTINUE                                 00007600
MSIG#1                                     00007610
NSIG#15                                    00007620
CALL SIGF2(CHL)                            00007630
CALL SIGF2(ASHIMB)                          00007640
CALL SIGF2(ASHIMC)                          00007650
CALL SIGF2(EJT)                            00007660
CALL SIGF2(BVUG)                           00007670
CALL SIGF2(TBL)                            00007680
CALL SIGF2(AXBL)                           00007690
DO 1035 I=1,15                                00007700
TOT(I)=CHL(I)+EJT(I)+TBL(I)+AXBL(I)+BVUG(I)+ASHIMC(I)+ASHIMS(I) 00007710
1035 CONTINUE                                 00007720
CALL SIGF2(TOT)                            00007730
WRITE(S1,906)                                00007740
WRITE(S1,905)NAME                           00007750
WRITE(S1,1051)                                00007760
1051 FORMAT(1H0,67X,'GASEOUS RELEASE RATE = CORIES PER     RTD) 00007770
WRITE(S1,1052)                                00007780
1052 FORMAT(1H0,11X,'PRIMARYT,4X,'SECONDARYT,7X,'GAS STRIPPING,11X, 00007790
1'BUILDING VENTILATION'12X,'COOLANT,5X,'COOLANT,5X,21T=1). 00007800
24X,30T=1),5X,1EL0DLAN AIR EJECTOR TOTAL/10X,'(MICRUCI/GH)(M00007810
3ICRUCI/GH SHUTDOWN CONTINUOUS REACTOR AUXILIARY TURBINE00007820
4 VENT OFFGAS EXHAUST) 00007830
WRITE(S1,1053)                                00007840
1053 FORMAT(1H0,----- 00007850
2-----) 00007860
1054 FORMAT(10 'AB,2(2X,1PE10,3),8(3X,1PE8,1,1X)) 00007870
GASTOT#0,0 00007880

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DO 490 I=1,13
 WRITE(51,1054)NUCLIV(I),CONCP(I),CONCS(I),ASHIMS(I),ASHINC(I),
 1CBL(I),AXBL(I),TBL(I),BVUG(I),EJT(I),TUT(I)
 GASTOT=GASTOT+TUT(I)
 490 CONTINUE
 DIV#10,**(INT(ALUG10(GASTOT))=1)
 GASTOT=INT(GASTOT/DIV+0.5)*DIV
 WRITE(51,1055) GASTOT
 1055 FORMAT(1H0,1 TOTAL NUCLEI GASEST,10IX,1PE8,1)
 DO 492 I=14,15
 WRITE(51,1054)NUCLIV(I),CONCP(I),CONCS(I),ASHIMS(I),ASHINC(I),
 1CBL(I),AXBL(I),TBL(I),BVUG(I),EJT(I),TUT(I)
 492 CONTINUE
 WRITE(51,215)IM3RLG
 WRITE(51,1053)
 WRITE(51,231)
 WRITE(51,906)
 WRITE(51,903)NAME
 WRITE(51,1060)
 WRITE(51,1061)
 WRITE(51,1053)
 1060 FORMAT(1H0,54X,'AIRBORNE PARTICULATE RELEASE RATE-CURIES PER YEAR'
 1)
 1061 FORMAT(1H0,36X,'WASTE GASF,16X,'BUILDING VENTILATION'/2X,'NUCLIDE'
 1,28X,'SYSTEM',14X,'REACTOR AUXILIARY',15X,'TOTAL')
 UH#8760,*UPFRAYEN
 DO 1070 I=1,8
 PRCONT(I)=PCHCP(I)/(1E3*8760.*UPFRAYEN)
 IF(PNUV.GT.0.0) GO TO 1067
 PCHCP(I)=0.0
 PCHSP(I)=EN*(PRCONT(I)*UHCSHEPA
 GO TO 1068
 1067 PCHCP(I)=EN*(UH*PRCONT(I)*PRCONT(I)/PNUV*(1.+EXP(-PNUV*EN)))
 1*CNHEPA
 PCHSP(I)=(EN*(PRCONT(I)/PNUV*(1.+EXP(-PNUV*EN))))*CSHEPA
 1068 PCBL(I)=PCHCP(I)+PCHSP(I)
 PAXBL(I)=PAXBP(I)/1E3*AXHEPA
 PGHL(I)=PGHS(I)/1E3*GHHEPA
 IF (KID,EQ,0) GO TO 1070
 POLAK=CFH*41.6/CONVUL
 PEXX2=POLAK*PURTIN
 IF(PEXX2.GT.,75.) PEXX2=75.
 PEXPF=EXP(-PEXX2)
 PEXPC=1.-PEXPF
 PELSS=PRCONT(I)/POLAK*PEXPC*LSHEPA
 PCBL(I)=PCHSP(I)*PEXPF+PELSS*EN+PCHCP(I)*(1.-PURTIN/(8760.*UPFRAYEN))
 IN)
 1070 CONTINUE
 NSIG#2
 NSIG#8
 CALL SIGF2(PCBL)
 DO 1075 I=1,8
 PTOTP(I)=PCBL(I)*PAXBL(I)*PGHL(I)
 1075 CONTINUE
 CALL SIGF2(PTOTP)
 DO 1076 I=1,8
 WRITE(51,1062)PAPART(I),PGHL(I),PCBL(I),PAXBL(I),PTOTP(I)
 1076 CONTINUE
 1062 FORMAT(1H0,48,28X,1PE8.1,11X,1PE8.1,4X,1PE8.1,15X,1PE8.1)
 WRITE(51,1053)
 GO TO 80
 00007920
 00007930
 00007940
 00007950
 00007960
 00007970
 00007980
 00007990
 00008000
 00008010
 00008020
 00008030
 00008040
 00008050
 00008060
 00008070
 00008080
 00008090
 00008100
 00008110
 00008120
 00008130
 00008140
 00008150
 00008160
 00008170
 00008180
 00008190
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 00008210
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 00008440
 00008450
 00008460
 00008470
 00008480
 00008490
 00008500
 00008510
 00008520

```

END
SUBROUTINE SIGF2(RLPT)
COMMON NSIG,NSIG
DIMENSION RLPT(NSIG)
IF (NSIG,EQ,2) GO TO 30
DO 20 I=1,NSIG
IF (RLPT(I),EQ,0.0) GO TO 20
IF (I,GT,13) GO TO 10
C THIS PART OF SUBROUTINE IS FOR NUCLE GASES
DIV#10,**(INT(ALUG10(RLPT(I)))-1)
IF (RLPT(I),LT,1.0) DIV#1.00
RLPT(I)=MAINT(RLPT(I))/DIV+0.5)*DIV
GO TO 20
C THIS PART OF SUBROUTINE IS FOR IONINE
10 CONTINUE
ISUB#2
IF(RLPT(I),GT,1.0)ISUB#1
DIV#10,**(INT(ALUG10(RLPT(I)))-ISUB)
RLPT(I)=MAINT(RLPT(I))/DIV+0.5)*DIV
20 CONTINUE
30 CONTINUE
C THIS PART OF SUBROUTINE IS FOR PARTICULATES
DO 50 I=1,NSIG
IF (RLPT(I),EQ,0.0) GO TO 50
DIV#10,**(INT(ALUG10(RLPT(I)))-2)
RLPT(I)=MAINT(RLPT(I))/DIV+0.5)*DIV
50 CONTINUE
RETURN
END

```

C GALE CODE FOR CALCULATING LIQUID EFFLUENTS FROM LWR'S. MODIFIED 000000010
C JULY 1975 TO IMPLEMENT APPENDIX I TO 10 CFR PART 50, REACTOR 00000020
C WATER CONCENTRATIONS CALCULATED USING METHODS OF DRAFT STANDARD 000000030
C AND 237 TRADECOTATIVE MATERIALS IN PRINCIPAL FLUID STREAMS OF 000000040
C LIGHT WATER COOLED NUCLEAR POWER PLANTS. DRAFT DATED MAY 20, 1974 000000050
C MODIFIED EDITION OF DRIGEN PROGRAM TO COMPUTE EFFLUENTS FROM BWR 000000060
C AND PWR RADIOTE SYSTEMS 000000070
C 000000080
C LOGICAL DISCHG,PINHRT 000000090
C INTEGER*2 LDC,NORDX,KD 00000100
C REAL*4 LETDXN,NGEN 00000110
C REAL*4 LETDXA 00000120
C REAL KKR,XKE,XNU,XMASS 00000130
C INTEGER*2 NAME(3) 00000140
C COMMON/MATRIX/A(2500),LDC(2500),NONR(800),KDE(800) 00000150
C COMMON/FLUX/FLUX(150),PNV,POUT,INDEX,NNX,NNY,ERR,NDBLD,IZERO 00000160
C COMMON/PROCESS/ MPRI(S,PRATE(R),NPRI(S,R),NZPHIS(R,20),PR(800)) 00000170
C COMMON/EQ/XZERO(800), XZH(800),XTEMP(KR01),XTEF(10,800), 00000180
C 1 R(800),DE800) 00000190
C COMMON/FLUXN/T(201,POWERT(10),TICAP(800),FISS(100),DIS(800),ILTTE, 00000200
C 1 TACT,TFP,TIT,TOK,INPT 00000210
C COMMON/OUT/NUCL(800),TITLE(20),UFR(800),FG(800),CUTOFF(7), 00000220
C 1 PDR,HURNUP,FLUXB,LSTAB,ALPHAN(100),SPONE(100),AHUND(800), 00000230
C 2 BASIS(10),TCNST,TUNIT 00000240
C COMMON/COND/PCOND(800),HCOND(800),CHCOND(800), 00000250
C 1 SCON(800),RKVCH(800) 00000260
C COMMON/COOL/REACTR,PI=1,TYPE,PCVHL,LETDXN,NDRAS,SCONL,STVOL,NGEN 00000270
C 1 ,NPURGE,NVLSPG,SHLR,GASOLA,STLKR,HLDRX,EJCTR,PLKRAT,00000280
C 2 GASLKR,CONDLP,TEHRRM,DFCBM,NZMRDM,NZCHDM,NE,PF, 00000290
C 3 STMFR,PFEP,HEF,DFCSH,DFCSB,DFELR,DFI,DFCS,DF, 00000300
C 4 ,DFFLR,DFIFD,DFCSED,DFED,DFELR,DFIOW,DFCSO,DFDN,DFDT 00000310
C 5 ,SRA,EOA,DNA,CFLR,CHFR,DXA,CHM,DFCH,DFID,DFCSH, 00000320
C 6 DFCH,DFICK,DFCSH,PHOLD,HHOLDE,HHOLDX,HHOLCH,PHOLDE 00000330
C 7 ,HDTFP,DFID,DFCSH,DFBD,HHDLDR,REGENT, 00000340
C 8 SHFD,DFMD,DFV,DFD,DFMD,DFYED,DFRBD,DFYDR, 00000350
C 9 DFMD,DFYHD,DFCN,DFHCR,DFYCH,CHFD,DFHCM,DFYCH 00000360
C A ,TS,TE,TD,TB,TC,TCH,TSTUR,TSTURD,TSTURH,TMSC,DAFL2,DW2,DHF2, 00000370
C B T2,TSTUR2,DFID2,DFCSO2,DFMD2,DFYD2,DFD2,PFIAIN 00000380
C COMMON/APCDBL/RGAFR,DFIRG,DFCSRG,DFRG,TRG,TSTURH,HGFD 00000390
C COMMON/BDTES/RFART 00000400
C COMMON/ZCONC/ZCONE(800) 00000410
C COMMON/COND/PCOND(800),SCUTV(800),SCUTP(800),SCUT(800) 00000420
C DIMENSION KR(01374), KRD15(8), KRD18(5), KRD23(6), KRD28(7), 00000430
C 1 KRD33(9), KRD10(3), KRD8(21), KRD40(10) 00000440
C DIMENSION REACTR(7),NZMRDM(26),NZCHDM(26) 00000450
C DIMENSION FACT(10),XCMP(200),INUEL(20) 00000460
C DATA YES/1YES1/ 00000470
C
C PCOND CONTAINS PRIMARY COOLANT CONCENTRATIONS FOR BWR'S. THE 00000480
C FOLLOWING ISOTOPES (WITH THEIR CONCENTRATIONS IN UCI/GHD) ARE 00000490
C ALSO PRESENT IN THE PRIMARY COOLANT BUT ARE NOT CONSIDERED 00000500
C SIGNIFICANT IN EFFLUENT CALCULATIONS: $N=13$, $O=5$, $S=16$, $H=17$, $P=9$, $F=19$, $Cl=18$, $K=10$, $Ca=14$, $Mg=12$, $B=11$, $Si=10$, $Na=9$, $Li=7$, $Rb=6$, $Br=5$, $As=4$. 00000510
C
C PCOND CONTAINS PRIMARY COOLANT CONCENTRATIONS FOR PWR'S. SCUTV, 00000530
C SCUTP, AND SCUT CONTAIN SECONDARY COOLANT CONCENTRATIONS FOR 00000540
C PLANTS WITH U-TUBE STEAM GENERATORS AND VOLATILE SECONDARY CHEM- 00000550
C ISTRY; FOR PLANTS WITH U-TUBE STEAM GENERATORS AND PHOSPHATE 00000560
C SECONDARY CHEMISTRY; AND FOR PLANTS WITH ONCE-THROUGH STEAM 00000570
C GENERATORS, RESPECTIVELY. 00000580
C DATA NTRY,INTER(0,0),PRH/I,PRH/I,PRH/I 00000590
C 00000600

```

C READ NUCLEAR DATA AND CONSTRUCT TRANSITION MATRIX
C
C 10 CALL NUDATA(NLKE)
C
C DO 20 I=2,NTOT
NNUC(I)=NUC(1)+NUC(I-1)
20 KDT1=KDT1+1,NNUC(I)
      DISCHG=.FALSE.
      PWRITE=.FALSE.
      K1=0
      INDEX=0
      RLXR=0.0
      PXRHEN=0.0
      BURN=0.0
      BUTFLR=1.0
      QXN=0.001
      AXN=ALOG(QXN)
      NEMITUT
      TCONSTABUNU=
      FDAO=0.0
      THSC=0.0
      TEE=0.0
      T5=0.0
      T2=0.0
      T8TIR2=0.0
      DWFLL2=0.0
      DW2=0.0
      DAF2=0.0
      DN=40 J=1,R0D
      PCNC(J)=0.0
      DCNC(J)=0.0
      SCNC(J)=0.0
      RTV(J)=0.0
      CNHC(J)=0.0
      CMNC(J)=0.0
      X2H(J)=0.0
      40 CONTINUE
C
C READ DESCRIPTION OF REACTOR AND RADIASTE TREATMENT PLANT
C
C DIMENSION NORD56(14)
      PRINT 9026
      READ 9010,REACTR,TYPE
      PRINT 9010,REACTR,TYPE
      READ 9011,NORD56,P01
      PRINT 9011,NORD56,P01
      PFM=0.80
      PRINT 9027
      IF(ETYPE.EQ.'BWR') GO TO 50
      C READ DATA FOR PWR LIQUID COOL
      READ 9022,NORD56,LETDA
      PRINT 9022,NORD56,PCVNL
      600 FAIL=0.12
      PRINT 9028,FAIL
      READ 9012,NORD56,LETDA
      PRINT 9012,NORD56,LETDA
      READ 9012,NORD56,CHFLR
      PRINT 9012,NORD56,CHFLR
      READ 9011,NORD56,NGFA
      PRINT 9011,NORD56,NGFA
      READ 9022,NORD56,STHFR

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PRINT 9022,WORD56,STMFR
 READ 9022,WORD56,WT
 PRINT 9022,WORD56,WST
 READ 9022,WORD56,WLI
 PRINT 9022,WORD56,WLI
 SCVOL=WORD56
 PRINT 9029,SCVIL
 READ 9011,WORD56,THSC
 PRINT 9011,WORD56,THSC
 READ 9055,BLDOWN,XFNRT
 PRINT 9051,BLNDAN
 RENRTAKENRT
 IF(RENRTAKENRT.GT.1.0) RENRTAKENRT=0
 PRINT 9041
 READ 9012,WORD56,REGENT
 PRINT 9012,WORD56,REGENT
 IF(BLDOWN,EW,0.0) GO TO 41
 FREFM0,001
 HEFM0,01
 PRINT 9030,FREF,HEF
 GO TO 44
 41 FREF#1,0
 HEF#1,0
 PRINT 9030,FREF,HEF
 44 CONTINUE
 READ 9020,WORD56,FFCDH
 PRINT 9020,WORD56,FFCDH
 IF(FFCDH.LT.0.001)GO TO 4444
 DFCBS#1,0
 DFCBCS#2,0
 GO TO 4445
 4444 DFCBS#1,0
 DFCBCS#1,0
 4445 CONTINUE
 READ 9011,WORD56,DILUT
 PRINT 9011,WORD56,DILUT
 READ 9058,WORD18,BLDH
 CHA#1,0
 READ 9014,DFICK,DFCSCH,DFCK
 READ 9015,TC,TSTORC,CFD
 PRINT 9045
 PRINT 9016
 PRINT 9017,WORD18,BLDH,CHA,CFD,TC,TSTORC,DFICK,DFCSCH,DFCK
 READ 9013,WORD18,DFELR,WORD8,EDA
 READ 9014,DFTEH,DFCSCH,DFED
 READ 9015,TE,TS,DFED
 PRINT 9017,WORD18,DFELR,EDA,DFED,TE,TS,DFTEH,DFCSCH,DFED
 READ 9013,WORD18,DFELR,WORD8,EDA
 READ 9014,DFTEH,DFCSCH,DFED
 READ 9015,TD,TSTORH,DFRD
 PRINT 9017,WORD18,DFELR,DA,DAFD,TD,TSTORH,DFIDA,DFCSCH,DFDX
 READ 9013,WORD18,DFELR,WORD8,D#2
 READ 9014,DFID2,DFCSCH,DFD#2
 READ 9015,T2,TSTORZ,DF#2
 PRINT 9017,WORD18,DFELR,D#2,D#2,T2,TSTORZ,DFID2,DFCSCH,DFD#2
 READ 9037,RDTER
 READ 9014,DFICK,DFCSCH,DFCK
 READ 9015,TCM,TSTORR,CFD
 READ 9037,RGWER
 READ 9014,DFIRG,DFCSRG,DFHG
 READ 9015,TRG,TSTORR,RGFD

IF(LEN(ENR,8),0,0) GO TO 45
 RDFFRSBLW\$=DATA1\$+RDFFRSBLW,3476
 PRINT 9034,RDFFRSBLW,TCM,TSTORH,DFICH,DFCSCH,DFCH
 RDFFRSBLW\$=DATA1\$+RDFFRSBLW,3476
 PRINT 9035,RDFFRSBLW
 IF(FFCDR,8,0,0) GO TO 46
 45 CONTINUE
 IF(FREGNT,8,0,0) GO TO 47
 PRINT 9038,RGAFR,RGFR,TRG,TSTORH,DFIRG,DFCSRG,DFRG
 GO TO 46
 47 RGAFR\$=0
 PRINT 9038,RGAFR,RGFR,TRG,TSTORH,DFIRG,DFCSRG,DFRG
 48 CONTINUE
 IF(ENR,8,0,0) GO TO 4446
 FNRTS\$=1,0=1,0/(DFCM*DFCH)
 FNRTS1\$=1,0=1,0/(DFICH*DFCH)
 FNRTSC\$=1,0=1,0/(DFCSCH*DFCH\$)
 GO TO 4447
 4446 FNRTS\$=1,0
 FNRTS1\$=1,0
 FNRTSC\$=1,0
 4447 CONTINUE
 C
 C READ DATA FOR HTR GAS CODE
 C
 PRINT 9046
 READ 9021,XGTRHT
 IF (XGTRHT,8,0,0) PRINT 9053
 IF (XGTRHT,8,11) PRINT 9052
 IF (XGTRHT,8,23) PRINT 9075
 READ 9012,HRD05A,TAU1
 PRINT 9012,HRD05B,TAU1
 READ 9012,HRD05A,TAU2
 PRINT 9012,HRD05B,TAU2
 READ 9012,HRD05C,TAU3
 PRINT 9012,HRD05E,TAU3
 GHEPAR\$=1,0
 FRIAR\$=1,0
 AXHEPAR\$=1,0
 FPFPE\$=1,0
 CSHEPAR\$=1,0
 FPPPE\$=1,0
 CNHEPAR\$=1,0
 READ 9065,HRD015,GHHT
 IF(GHHT,8,YES)GHEPAR\$=0,01
 PRINT 9066,HRD015,GHEPAR\$
 READ 9067,HRD018,AXCH,AXHT
 IF(AXCH,8,YES)FRTAHE\$=1
 IF(AXHT,8,YES)AXHEPAR\$=0,01
 PRINT 9068,HRD018,FHTAH,AXHEPA
 READ 9022,HRD05A,CNHEPA
 PRINT 9022,HRD05B,CNHEPA
 READ 9022,HRD05B,CFP
 PRINT 9022,HRD05B,CFP
 READ 9071,HRD018,CSCH,CSHT,ENP
 IF(CSCH,8,YES)FPPPE\$=1
 IF(CSHT,8,YES)TSHEPAR\$=0,01
 ENP\$=0\$ENP\$
 PRINT 9072,ENP\$
 PRINT 9068,HRD018,FPPPE,CSHEPA
 READ 9069,HRD018,PHIV1,CNCH,CHHT

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IF(CNCH,EQ,YES)PFRN=0.1
IF(CNHT,EQ,YES)CNH=PA=0.01
IF (PNOV<LT,1,0) GO TO 4448
PRINT 9070,XORD18,PNOV1,XRD18,FPRN,CNHPA
GO TO 4449
4448 PRINT 9073
4449 CONTINUE
      TALK#1700,
      PRINT 9064,THLK
      READ 9020,XRD058,FVN
      PRINT 9020,XRD058,FVN
      READ 9020,XRD058,FEJ
      PRINT 9020,XRD058,FEJ
      KCRYD0=0
      IF(KCRYD0,NE,0,0) GO TO 48
      PRINT 9039
      GO TO 49
48 PRINT 9040
49 CONTINUE
      READ 9020,XRD058,PFLAUN
      IF(PFLAUN,LE,0,0) PRINT 9048
      PRINT 9026
C
C CONVERSION OF UNITS
C
      EDFLR=EDFLR*48.8
      DFLRBD=FLR*48.8
      DFLZBD=FLZ*48.8
      GO TO 240
C
C READ DATA FOR BKR LIQUID CODE
C
50 READ 9022,XRD058,STHFR
      PRINT 9022,XRD058,STHFR
      READ 9022,XRD058,PCVOL
      PRINT 9022,XRD058,PCVOL
      PREFEN=0.01
      HRF=0.020
      PRINT 9030,FREF,HFF
      READ 9022,XRD058,LETDAH
      PRNT 9022,444756,LETDAH
      READ 9022,XRD058,REGENT
      PRNT 9022,XRD058,REGENT
      READ 9022,XRD058,FFCDH
      PRNT 9022,XRD058,FFCDH
      READ 9022,XRD058,DILUT
      PRNT 9022,XRD058,DILUT
      PRINT 9045
      READ 9013,XORD18,CFPLR,DFRDB,CHA
      READ 9014,DFICM,DFCSCH,DFCH
      READ 9015,TC,TSTDRH,CFD
      PRINT 9016
      PRINT 9017,XORD18,CFPLR,CHA,CFRD,TC,TSTDRH,DFICM,DFCSCH,DFCH
      READ 9013,XORD18,CFPLR,DFRDB,DHA
      READ 9014,DFIDW,DFCSCH,DFCH
      READ 9015,TC,TSTDRH,DHA
      PRINT 9017,XORD18,CFPLR,DHA,DFIDW,TC,TSTDRH,DFICM,DFCSCH,DFCH
      READ 9013,XORD18,CFHFR,XRD058,CHA
      READ 9014,DFICM,DFCSCH,DFCH
      READ 9015,TC,TSTDRH,CFD
      PRINT 9017,XORD18,CFHFR,CHA,CFRD,TC,TSTDRH,DFICM,DFCSCH,DFCH

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READ 9037, RGAFF
 READ 9014, DFIRG, DFCSRG, DRFG
 READ 9015, TRG, TSTERR, RGFD
 PRINT 9038, RGAFR, RGFD, TRG, TSTERR, DFIRG, DFCSRG, DRFG
 E
 E
 E
 READ DATA FOR BHR GAS CODE
 PRINT 9046
 READ 9022, XRD58, GGS
 PRINT 9022, XRD58, GGS
 READ 9022, XRD58, -STE
 PRINT 9022, XRD58, -STE
 READ 9011, XRD58, TIM3
 PRINT 9011, XRD58, TIM3
 READ 9011, XRD58, TIMA
 PRINT 9011, XRD58, TIMA
 HEPAl#1, 0
 FIL1#1, 0
 HEPa2#1, 0
 FIL2#1, 0
 HEPa5#1, 0
 FIL5#1, 0
 HEPa6#1, 0
 FIL6#1, 0
 CSRF#1, 0
 READ 9060, XRD015, CHCH, CRHEPA
 IF(CRCH, EQ, YES) FIL1#1, 1
 IF(CRHEPA, EQ, YES) HEPAl#0, 01
 PRINT 9061, XRD015, FIL1, HEPAl
 READ 9062, XRD015, TRCH, THHEPA, TRCS
 IF(TRCH, EQ, YES) FIL2#0, 1
 IF(TRHEPA, EQ, YES) HEPa2#0, 01
 IF(TRCS, EQ, YES) CSRF#0, 2
 PRINT 9063, XRD015, FIL2, HEPa2, CSRF
 READ 9022, XRD58, FIL3
 PRINT 9022, XRD58, FIL3
 READ 9022, XRD58, FIL4
 PRINT 9022, XRD58, FIL4
 READ 9060, XRD015, AXCH, AXHEPA
 IF(AXCH, EQ, YES) FIL5#0, 1
 IF(AXHEP, EQ, YES) HEPa5#0, 01
 PRINT 9061, XRD015, FIL5, HEPa5
 READ 9061, XRD015, RACH, RAHEPA
 IF(RAHC, EQ, YES) FIL6#0, 1
 IF(RAHEPA, EQ, YES) HEPa6#0, 01
 PRINT 9061, XRD015, FIL6, HEPa6
 READ 9021, KCHAR
 READ 9012, XRD58, XKR
 READ 9011, XRD58, XKE
 READ 9012, XRD58, XNO
 READ 9022, XRD58, XMASS
 IF(KCHAR, EQ, 01) GO TO 54
 IF(KCHAR, EQ, 11) GO TO 55
 PRINT 9023
 GO TO 56
 54 PRINT 9024
 GO TO 56
 55 F=10, XNO
 CHTI1=(0.53*KKR*XMASS)/(F*24,*2.)
 CHTI2=(0.53*XXE*XMASS)/(F*24,*2.)
 PRINT 9025, KKR, XKE, XNO, XMASS, CHTI1, CHTI2

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56 CONTINUE
  READ 9020, KORD56, PFLAUN
  IF(PFLAUN.LE.0.0) PRINT 9048
  PRINT 9026
57 DO 58 J=1,ITOT
  BETI=0.0
58 CONTINUE
C
  DFIED=1,
  DFCSED=1,
  DFED=1,
  DFID2=1,
  DFCSD2=1,
  DFD2=1,
240 CONTINUE
C
C   CALCULATE PRIMARY COOLANT CONCENTRATIONS FOR PRRS
C
  IF(CTYPE.EQ.BHRIGD) GO TO 251
  AFRTE3=0.0
  DO 242 I=1,ITOT
242 PCONC(I)=PFCONC(I)
  POWA=POA1
  PCVDA=PCVOL*1E3
  LETD=LETDRN*500.53
  SBLDA=SBLDR*3478
  CBFLA=CBFLR*500.53
C
C   CHECK TO SEE IF PRIMARY PLANT PARAMETERS ARE WITHIN SPECIFIED
C   RANGES
  IF(ARS(PDWA=3400),GT,400,1)GO TO 243
  IF(ARS(PCVDA=5.5E5),GT,0.5001E5)GO TO 243
  IF(ARS(LETDR=3.7E4),GT,0.5001E4)GO TO 243
  IF(ARS(SBLDA=625.),GT,375.1)GO TO 243
  IF(ARS(CBFLA=3750.),GT,3750.1)GO TO 243
  GO TO 247
C
C   CALCULATE PRR PRIMARY COOLANT ADJUSTMENT FACTORS
  243 AFRTE3=1.0
  RHAL2=(LETD+4*0.9+0.1*SBLDA)/PCVDA
  RCSRK2=(LETDR*0.5+0.5*(SBLDA+CBFLA*0.9))/PCVDA
  RCFF2=(LETD*0.9+0.1*(SBLDA+CBFLA*0.9))/PCVDA
  RK2=161.76*POA1/PCVDA
  DO 248 J=1,ITOT
  IF(PCONC(J).EQ.0.0) GO TO 248
  NZ=NICL(J)/10000
  DL=DIS(J)*3600.
  IF(NZ.EQ.53.0R.NZ.EQ.35)GO TO 248
  IF(NZ.EQ.37.0R.NZ.EQ.55)GO TO 245
  PCONC(J)=PCONC(J)*RK2*(0.0612+DL)/(RCFF2+DL)
  GO TO 248
244 PCONC(J)=PCONC(J)*RK2*(0.0608+DL)/(RHAL2+DL)
  GO TO 248
245 PCONC(J)=PCONC(J)*RK2*(0.0371+DL)/(RCSRK2+DL)
246 CONTINUE
247 SBLDR=SBLDR*GR.8
  PCVOL=PCVOL*1000.*0.7/82.4
C
C   CALCULATE PRR SECONDARY COOLANT CONCENTRATIONS
  SCVDA=SCVOL*1E3
  BLNDRA=BLNDRN*1E3
  STMFA=STMFR*1FB
  FFCDA=FFCOM
C
C   CHECK TO SEE IF SECONDARY PLANT PARAMETERS ARE WITHIN SPECIFIED

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RANGES
1 IF(BLWDHN.EQ.0,0) GO TO 263
1 IF(PYFCDA.LE.0,0) GO TO 261
PYTYPE2=0 IS A PLANT WITH U-TUBE STEAM GENERATORS AND VOLATILE
SEPODARY CHEMISTRY
PYTYPE=2,0

DO 260 IM1,ITOT
260 SCON(1)*SCON(1) GO TO 266
IF(CAPTES.EQ.1,0) GO TO 266
IF(ABS(SCVDA=4.5E5).GT.0.5001E5/30) GO TO 266
IF(ABS(STHFA=1.5E7).GT.0.2001E7) GO TO 266
IF(ABS(BLWDHA=7.5E4).GT.2.5001E4) GO TO 266
IF(ABS(FPCDA=0.65).GT.0.10001) GO TO 266
IF(PNRTSC.LT.0.89999) GO TO 2278
GO TO 278

PYTYPE1=0 IS A PLANT WITH U-TUBE STEAM GENERATORS AND PHOSPHATE
SECONDARY CHEMISTRY
261 PYTYPE3,0
DO 262 IM1,ITOT
262 SCON(1)*SCUTP(1)
IF(PNTYPE3.EQ.1,0) GO TO 266
IF(ABS(SCVDA=4.5E5).GT.0.5001E5/30) GO TO 266
IF(ABS(STHFA=1.5E7).GT.0.2001E7) GO TO 266
IF(ABS(BLWDHA=9E3).GT.1.0E3) GO TO 266
IF(ABS(FPCDA=.005).GT.0.005001) GO TO 266
IF(PNRTSC.LT.0.89999) GO TO 2278
GO TO 278

PYTYPE1=0 IS A PLANT WITH ONCE-THROUGH STEAM GENERATORS
263 PYTYPE1,0
DO 264 IM1,ITOT
264 SCON(1)*SCOT(1)
IF(PNTYPE1.EQ.1,0) GO TO 266
IF(ABS(STHFA=1.5E7).GT.0.2001E7) GO TO 266
IF(ABS(FPCDA=0.65).GT.0.10001) GO TO 266
GO TO 278

CALCULATE PHR SECONDARY COOLANT ADJUSTMENT FACTORS
266 RHAL3*(BLWDHA*PNRTSC+0.9*HEPEPSTHFA*FPCDA)/SCVDA
RC5R83*(BLWDHA*PNRTSC+0.5*HEPEPSTHFA*FPCDA)/SCVDA
RCPP3*(BLWDHA*PNRTSC+0.9*HEPEPSTHFA*FPCDA)/SCVDA
IF(PNTYPE1.EQ.1,0) GO TO 274
RK3*4.5E5/SCVDA
IF(PNTYPE2.EQ.2,0) GO TO 270
DO 269 IM1,ITOT
IF(SCON(1),EQ,0,0) GO TO 269
NZ=NUCL(1)*10000
DLNDIS(1)=30000
IF(NZ.EQ.51,OR,NZ.EQ.35) GO TO 267
IF(NZ.EQ.37,OR,NZ.EQ.55) GO TO 268
SCON(1)*SCON(1)*RK3*(.02+DL)*(PCHCONC(1)/PHCONC(1))
GO TO 269
267 SCON(1)*SCON(1)*RK3*(.02+DL)*(PCHCONC(1)/PHCONC(1))
GO TO 269
268 SCON(1)*SCON(1)*RK3*(.02+DL)*(PCHRB3*DL)*(PCHCONC(Y)/PHCONC(1))
269 CONTINUE
GO TO 278
270 CONTINUE
DO 273 IM1,ITOT
IF(SCON(1),EQ,0,0) GO TO 273
NZ=NUCL(1)*10000
DLNDIS(1)=30000
IF(NZ.EQ.51,OR,NZ.EQ.35) GO TO 271

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IP(NZ.EQ.37.OR.NZ.EQ.55)GO TO 272
SCON(I)*SConC(I)*Rk3*(0.1862+DL)/(RCFP3+DL)*(PConC(I)/PConC(I))
GO TO 273
271 SCON(I)*SConC(I)*Rk3*(0.3617+DL)/(RHAL3+DL)*(PConC(I)/PConC(I))
GO TO 273
272 SCON(I)*SConC(I)*Rk3*(0.1775+DL)/(RC8RB3+DL)*(PConC(I)/PConC(I))
GO TO 273
CONTINUE
273 GO TO 278
274 RK3*E5/SCVOA
IF(SCon(I).EQ.0.)GO TO 274
NZ=NUCL(I)/1000
DLDISC(I)*3600
IP(NZ.EQ.53.OR.NZ.EQ.35)GO TO 275
IP(NZ.EQ.55.OR.NZ.EQ.37)GO TO 276
SCON(I)*SConC(I)*Rk3*07.75/RCFP3*(PConC(I)/PConC(I))
GO TO 277
275 SCON(I)*SConC(I)*Rk3*67.75/RHAL3*(PConC(I)/PConC(I))
GO TO 277
276 SCON(I)*SConC(I)*Rk3*48.75/RC8RB3*(PConC(I)/PConC(I))
CONTINUE
277 GO TO 278
278 RC8RB3*(BLNDHAWNRTSC+0.5*PPPEMSTHAPPFCDA)/SCVOA
RK3*4.5E5/SCVOA
DO 2279 I=1,ITOT
IP(SCon(I),EQ.0.)GO TO 2279
NZ=NUCL(I)/1000
IF(NZ.NE.37.AND.NZ.NE.55) GO TO 2279
DLDISC(I)*3600.
RSC=.02
IP(PHTYPE.EQ.2.0) RSC=.1775
SCON(I)*SConC(I)*Rk3*(RSC+DL)/(RC8RB3+DL)*(PConC(I)/PConC(I))
CONTINUE
2279 SCVOL=SCVOL*1000./62.4
STPHRMFR=2000.
DO 279 I=1,ITOT
IP(PConC(I),EQ.0.)GO TO 279
PConC(I)*PConC(I)/(DIS(I)*1.6283E13)
SCON(I)*SConC(I)/(DIS(I)*1.6283E13)
CONTINUE
279 COMPUTE REMOVAL CONSTANT FOR CONDENSATE DEMINERALIZER IN PHR
C IP(REGENT.GE.0.0) GO TO 300
CALL EPFTAB
GO TO 30
300 CIIRC=(0.9*BLNDHAWNRT/DFCH+0.9*8THRF*PFPCDM)/(SCVOL*.48*60.0)
1 CIYRC=(0.5*BLNDHAWNRT/DFCSCH+0.5*STHFR*PFPCDM)/(SCVOL*.7*.48*60.0)
2 60.* CIYRIB=(0.9*BLNDHAWNRT/DFICH+0.9*STHFR*HEFPPFCDM)/(SCVOL*.7*.48*60.0)
3 0005430
4 0005340
5 0005350
6 0005360
7 0005370
8 0005380
9 0005390
PR(I)*CIIRC
IP(NZ.EQ.37.OR.NZ.EQ.55)PR(I)*CIIRC
IP(NZ.EQ.53.OR.NZ.EQ.35)PR(I)*CIYRIB
XHZJ=SConC(I)*PR(I)*SCVOL*.02832
B(I)=XHZJ
XHZ(I)=XHZJ*86400.
XZPRO(I)=0.

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305 CONTINUE
C   CALCULATE RADIOISOTOPES INVENTORIES ON PAR CONDENSATE RESINS      00005540
T(1)*REGENT
CALL SOLVE
DO 330 I=1,ITUT
330 RINV(I)=XTEHR(I)
CALL EFFTAB
GO TO 30
C
C
251 CONTINUE
C   CALCULATE PAR PRIMARY COOLANT CONCENTRATIONS      00005600
DO 2251 I=1,ITUT
2251 PCONC(I)=BC/MC(I)
PCV0=PCVUL*1E6
LETDRH=LETDRH*1E6
STMFR=STMFR*1E6
FFCDR=FFCDM
C   CHECK TO SEE IF PLANT PARAMETERS ARE WITHIN SPECIFIED RANGES      00005640
IF(AHS(POA)=3400),GT,400,1)GO TO 252
IF(AHS(PCV0A=3,RF5),GT,0,4001F5)GO TO 252
IF(AHS(LETDRH=1,3F5),GT,0,2001F5)GO TO 252
IF(AHS(STMFR=1,SE7),GT,0,2001E7)GO TO 252
IF(AHS(FFCDR=0,9),GT,0,1001)GO TO 252
GO TO 256
C   CALCULATE HTR ADJUSTMENT FACTORS      00005700
252 RHAL2=(LETDRH*0,9+FFCDR*STMFR*0,01R)/PCV0A
RC8RH2=(LETDRH*0,5+FFCDR*STMFR*5E-4)/PCV0A
RCFP2=(LETDRH*0,9+FFCDR*STMFR*0E-4)/PCV0A
RK2=111,76PCV0A/PCV0A
DO 255 J=1,ITUT
IF(PCONC(J),EQ,0,0) GO TO 255
NZNUCL(J)/10000
DLBDISC(J)*3600
IF(NZ,ER,53,0R,NZ,ER,35)GO TO 253
IF(NZ,ER,37,0R,NZ,ER,55)GO TO 254
PCONC(J)=PCONC(J)*RK2*(0,3434+DL)/(RCFP2+DL)
GO TO 255
253 PCONC(J)=PCONC(J)*RK2*(0,1908+DL)/(RC8RH2+DL)
GO TO 255
254 PCONC(J)=PCONC(J)*RK2*(0,1908+DL)/(RC8RH2+DL)
255 CONTINUE
256 PCV0L=PCV0L*1000000./62,4
LETDRH=LETDRH*2000.
STMFR=STMFR*2851,
DO 2255 J=1,ITUT
IF((PCONC(J),GT,0,0)PCONC(J)*PCONC(J)/(DL*(J)*1,6283E13))
2255 CONTINUE
IF(REGENT,GT,0,0) GO TO 257
CALL EFFTAB
GO TO 30
C
C
COMPUTE REMOVAL CONSTANT FOR CONDENSATE DEMINERALIZER IN HTR      00006000
257 CCBDM=0,R*STMFR*PREF/(PCV0L*7,48*80,)*FFCDM      00006070
CSBDM=0,5*STMFR*PREF/(PCV0L*7,48*80,)*FFCDM      00006080
DO 258 I=1,ITUT
NZNUCL(I)/10000
PRE(I)=CCBDM
IF(NZ,ER,53,0R,NZ,ER,35)PRE(I)=CCBDM*HEF/PREF
IF(NZ,ER,37,0R,NZ,ER,55)PRE(I)=CSBDM      00006090
DO 258 I=1,ITUT
NZNUCL(I)/10000
PRE(I)=CCBDM
IF(NZ,ER,53,0R,NZ,ER,35)PRE(I)=CCBDM*HEF/PREF
IF(NZ,ER,37,0R,NZ,ER,55)PRE(I)=CSBDM      00006100
DO 258 I=1,ITUT
NZNUCL(I)/10000
PRE(I)=CCBDM
IF(NZ,ER,53,0R,NZ,ER,35)PRE(I)=CCBDM*HEF/PREF
IF(NZ,ER,37,0R,NZ,ER,55)PRE(I)=CSBDM      00006110
DO 258 I=1,ITUT
NZNUCL(I)/10000
PRE(I)=CCBDM
IF(NZ,ER,53,0R,NZ,ER,35)PRE(I)=CCBDM*HEF/PREF
IF(NZ,ER,37,0R,NZ,ER,55)PRE(I)=CSBDM      00006120
DO 258 I=1,ITUT
NZNUCL(I)/10000
PRE(I)=CCBDM
IF(NZ,ER,53,0R,NZ,ER,35)PRE(I)=CCBDM*HEF/PREF
IF(NZ,ER,37,0R,NZ,ER,55)PRE(I)=CSBDM      00006130
DO 258 I=1,ITUT
NZNUCL(I)/10000
PRE(I)=CCBDM
IF(NZ,ER,53,0R,NZ,ER,35)PRE(I)=CCBDM*HEF/PREF
IF(NZ,ER,37,0R,NZ,ER,55)PRE(I)=CSBDM      00006140

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XZHJ*PCOND(I)*PH(I)*PEVOL=0.02832
 R(I)=XZHJ
 XZH(I)=XZHJ*86400.
 258 CONTINUE
 XZERO(I)=0.
 C CALCULATE INVENTORIES OF EXR CONDENSATE RESTNS
 290 T(1)=REGENT
 CALL SOLVE
 DO 295 I=1,ITOT
 295 RINV(I)=XTEMP(I)
 CALL EFTTAB
 GO TO 30
 C
 C FORMATS FORMATS FORMATS
 C
 9000 FORMAT(20A4)
 9001 FORMAT(10E8.2)
 9002 FORMAT(8E10.3)
 9003 FORMAT(5(1E,F9.2),1S)
 9004 FORMAT(16I5)
 9005 FORMAT('0MMN OR MOUT EXCEEDS DIMENSION\$')
 9006 FORMAT('MOUT SHOULD NOT EXCEED MMN BY MORE THAN 10%')
 9007 FORMAT(E8.2,I2))
 9008 FORMAT(20I4)
 9009 FORMAT(10A4,F7.0,A3,F10.3)
 9010 FORMAT(32X,7A4,16X,A4)
 9011 FORMAT(16X,13A4,A3,F9.0)
 9012 FORMAT(16X,14A4,F9.0)
 9013 FORMAT(15X,4A4,A2,BX,FR.0,1X,A4,A2,FS,3)
 9014 FORMAT(20X,F8.0,27SX,FR.0))
 9015 FORMAT(27X,F6.2,10X,F6.2,1HX,F6.2)
 9016 FORMAT(10!,30X,1FRACTION, FRACTION, COLLECTION, DECAY!,BX,1STREAM 00006460
 1 FLOW RATE OF PCA DISCHARGED TIME TIME!,10X,1DECONT&00006470
 2MULTIPLICATION FACTORS!,20X,1(GAL/DAY)!23X,1(DAYS)!,7X,
 311!,RX,1CSI!,BY,1THERST!)
 9017 FORMAT(2X,4A4,A2,1PE9.2,1X,4(0PF8.3,2X),3(1PE9.2,1X))
 9020 FORMAT(16X,14A4,FR.4)
 9021 FORMAT(79X,T1)
 9022 FORMAT(16X,14A4,FR.4)
 9023 FORMAT(16X,1THERE IS A CRYOGENIC DISTILLATION COLUMN!,20X,1DDTIME 00006540
 1AND XENON DECONTAMINATION FACTORY!,T71,110000,1/20X,1KRYPTON DECONT&00006550
 2DISTILLATION FACTORY!,T72,14000,1/20X,1KRYPTON AND XENON HOLDUP TIME (00006560
 3DAYS!),T74,190,13
 9024 FORMAT(16X,1THERE IS NO CHARCOAL DELAY SYSTEM!) 00006580
 9025 FORMAT(16X,1THERE IS A CHARCOAL DELAY SYSTEM!,20X,1KRYPTON DYNAMIC!C00006590
 1 ADSORPTION COEFFICIENT (CM³/GM)!,T72,F9.4/20X,1XENON DYNAMIC ADS000006600
 2REPTION COEFFICIENT (CM³/GM)!,T72,F9.4/20X,1NUMBER OF MAIN CONDENSES!00006610
 3R SHELLS!,T72,F9.4/20X,1MASS OF CHARCOAL (SHORT TONS)!,T72,FR.0X 00006620
 420X,1KRYPTON HOLDUP TIME (DAYS)!,T72,F9.4/20X,1XENON HOLDUP TIME (00006630
 5DAYS!),T72,F9.4) 00006640
 9026 FORMAT(1H1) 00006650
 9027 FORMAT(16X,1PLANT CAPACITY FACTORY!,T75,T0,B0) 00006660
 9028 FORMAT(16X,1PERCENT FUEL WITH CLADDING DEFECTS!,T75,F6.4) 00006670
 9029 FORMAT(16X,1MASS OF WATER IN STEAM GENERATORS (THOUSAND LBS)!,T73,00006680
 1FB,4) 00006690
 9030 FORMAT(16X,1FISSION PRODUCT CARRYOVER FRACTION!,T75,F6.4/16X, 00006700
 1HALOGEN CARRYOVER FRACTION!,T75,F6.4) 00006710
 9032 FORMAT(2X,7A4,F7.0,3A4,A1,FS,3,3A4,A3,I2,244) 00006720
 9034 FORMAT(2X,1BLANKLINE!,10X,1PE9.2,14X,0PF5.3,2X,2(F8.3,2X),
 13(1PE4.2,1X)) 00006730
 9035 FORMAT(2X,1UNTREATED BLOWDOWN!,1PE9.2,11X,1 1,000 0.0 00006750

10,0 1,00E 00 1,00E 00 1,00E 00
 9036 FORMAT(16X, 'THERE IS NOT A CONDENSATE DEMINERALIZER') 000068780
 9037 FORMAT(72X,FR,,2)
 9038 FORMAT(2X,TREGENERANT SOLS 1,1PER9,2,14X,0PFS,3,2X,2(FR,3,2X),
 13(1PER9,2,1X)) 000068790
 9039 FORMAT(16X, 'THERE IS A CRYOGENIC OFFGAS SYSTEM') 000068810
 9040 FORMAT(16X, 'THERE IS NO CRYOGENIC OFFGAS SYSTEM') 000068820
 9041 FORMAT(16X,IP <INHAR TO SECONDARY LEAK RATE (LBS/DAY)),T73,T100,*) 000068830
 9045 FORMAT (/,10 LIQUID WASTE INPUTS) 000068840
 9046 FORMAT (/,10 GASEOUS WASTE INPUTS) 000068850
 9048 FORMAT(10!,15X, 'THERE IS NOT AN ONSITE LAUNDRY') 000068860
 9051 FORMAT(16X,FLUIDLOSS RATE (THOUSAND LBS/HRT),25X,F14,4) 000068870
 9052 FORMAT(16X, 'THERE IS CONTINUOUS STRIPPING OF FULL LIQUIDAN FLOWS') 000068880
 9053 FORMAT (16X, 'THERE IS NOT CONTINUOUS STRIPPING OF FULL LIQUIDAN FLOW') 000068890
 1)
 9054 FORMAT(16X,FLUX RATE THROUGH GAS STRIPPER (GPM),1,20X,F8,4) 000068910
 9055 FORMAT(36X,FR,4,35X,T1)
 9056 FORMAT(15X,440,A2,BX,FR,,0)
 9060 FORMAT (16X,044,10X,A3,6X,A5) 000068940
 9061 FORMAT (16X,444,1IODINE RELEASE FRACTION),16X,F10,5/32X,TPARTICULAT000068950
 1E RELEASE FRACTION,10X,F10,5) 000068960
 9062 FORMAT(16X,444,10X,A3,6X,A3,13X,A5) 000068970
 9063 FORMAT(16X,444,1IODINE RELEASE FRACTION),16X,F10,5/32X,TPARTICULAT000068980
 1E RELEASE FRACT(10!,10X,F10,5/32X,1RELEASE FRACT.=SPECIAL DES. FFA000068990
 2THRES!,1X,F10,5) 000070000
 9064 FORMAT(16X,1STEAM LEAK TO TURBINE HLDG (LBS/HRT),19X,F10,5) 000070100
 9065 FORMAT(16X,444,6X,A5) 000070200
 9066 FORMAT(16X,544,4X,1PARTICULATE RELEASE FRACTION),6X,F10,5) 000070300
 9067 FORMAT(16X,544,10X,A3,6X,A5) 000070400
 9068 FORMAT(16X,544,1IODINE RELEASE FRACTION),11X,F10,5/36X,TPARTICULAT000070500
 1E RELEASE FRACTION,6X,F10,5) 000070600
 9069 FORMAT(16X,544,9X,FR,2,9X,A3,6X,A3) 000070700
 9070 FORMAT(16X,544,1RATE(CR-),1,27X,FR,2/1AX,544,1IODINE RELEASE FRACTION)000070800
 1DN!,11X,F10,5/36X,TPARTICULATE RELEASE FRACTION),6X,F10,5) 000070900
 9071 FORMAT(16X,544,10X,A3,6X,A3,19X,F3,0) 000071000
 9072 FORMAT (16X,1FREQUENCY OF CHTHT HLDG HIGH VOL PURGE (TIMES/YR),
 1774,FB,,0) 000071100
 9073 FORMAT (16X, 'THERE IS NOT A CHTHT HLDG LOW VOL PURGE') 000071300
 9075 FORMAT(16X, 'THERE IS CONTINUOUS LOW VOL PURGE OF VOL. CONTROL TK')100007135
 END
 SUBROUTINE EFFTAH
 INTEGER,PARAMETER
 NAME(3)
 DIMENSION NZMRDM(26),NZCBDM(26),REACTR(7)
 DIMENSION TURBIR(800),DADCR(800),EDCOND(800)
 DIMENSION LAUNDRY(12),LAUND(12)
 COMMON/ZERO/XZERO(800), XZHR(800), XTEHR(800), XHEH(10,800),
 1 B(800),R(800)
 COMMON/FLUXN/T(20),P0=FR(10),TOCAP(800),FTSS(100),DIST800),ILITE,
 1 IACT,IPF,ITOT,AGN,INPT 000071400
 COMMON/VOL/NUCL(800),TITLE(20),R(800),FG(800),CUTOFF(7),
 1 P0X,BURNUP,FLUXR,MSTAR,ALRMA=(100),SPOND(100),ABUND(500),
 2 BASIS(10),TCNST,TUNIT
 COMMON/CODE/RADACT,POW!,TYPE,PCVOL,LETOWN,NUGAS,SCVUL,STHVL,NGEN00007270
 1 ,NPURGE,NVCEPG,SHLR,GASOLU,STLKR,BLDRH,EJCTR,ALKRAT,00007280
 2 ,GASLR,CUNLR,DFMRDM,DFCBDM,AZMHDN!,AZCBDM,NE,PF,
 3 ,STMR,PFEP,HEF,PECDM,DFMBCS,CHFLR,DFI,DFCS,DF,
 4 ,DFFLR,DIED,DFCSER,DFAD,DFFLR,DTDR,DFCSDA,DFDA,DFLUT 000072900
 5 ,BRA,EDR,DRW,CFRLR,CMRFR,DRX,CHAF,DFCM,DFICH,DFCSCM,
 6 ,DFCA,DFICH,DFCSC,PHOLDU,MHOLDE,MHOLDW,MHOLCH,MHOLDC 000073200
 7 ,PHOTR,DFIRD,DFCSRD,DFHD,MHOLDR,REGENT,
 8 ,SBFD,DFMO,DFV,EDFD,DFMD,DFYED,DFHD,DFHODA,DFHDW, 000073400
 9 ,SBFD,DFMO,DFV,EDFD,DFMD,DFYED,DFHD,DFHODA,DFHDW, 000073500

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9      OFXHDF,OFYHDF,OFZHDF,OFXHCK,OFYHCK,OFZHCK,OFXCH      00007380
8      ,TRATE,TD,TH,TC,TCH,TSTORC,TSTIRD,TSTIRB,THSC,DWFL2,DX2,DXF2,      00007370
9      T2,TSTOR2,DF102,DFCSR2,DFHDF2,DFYD2,DFD2,PFLAU      00007380
COMMON/APC001/RGFR,DFIRG,DFCSRG,DFRG,TRG,TSTORR,RGEF      00007390
COMMON/BOTES/RFNRT      00007400
COMMON/FLEX/FLEX(10),RHN,ROUT,INDEX,DXN,AXN,ERR,NOBLND,HZERO      00007405
COMMON/CINC/PCINC(B001),DXCINC(B001),DXCONC(B001),DXCOND(B001),      00007420
1      SCUN(B001),RINV(B001)      00007430
COMMON/MPCTAB,AMPC(B001),AMPC(B002)      00007440
EQUIVALENCE (XZERO(1)),TURBINE(1), (XZH(11),DXCON2(1))      00007450
DATA PHAT PHAT, HART / HART /
DATA LAUNDRY/250580,270580,270600,400950,410950,441030,441060,      00007470
1      471101,531310,551340,551370,581440/      00007480
DATA XLAUND/0.001,0.004,0.0087,0.0014,0.002,0.00014,0.0024,      00007490
1      0.00044,0.000062,0.013,0.024,0.0052/      00007500
DO 10 IT1,ITUT      00007510
10     D(IJ)=DIS(IJ)      00007520
IF(TYPE,EQ,BAR) GO TO 15      00007530
H3PRPH=0,4*PI*A      00007540
C      H3PRPH IS THE BAR TRITIUM PRIMARY COOLANT CONCENTRATION IN      00007550
C      UCI/GM      00007560
H3CPH=1.0      00007570
C1=SALDR*CNA      00007580
C2=EDFLR*CNA      00007590
C1*C1/(C1+C2)      00007600
C2=1.-C1      00007610
GO TO 20      00007620
C      TRITCO IS THE BAR TRITIUM PRIMARY COOLANT CONCENTRATION IN      00007630
C      UCI/GM.      00007640
15     TRITPH=.025*PI*A      00007650
TRITCH=.01      00007660
20     DO 30 J=1,ITOT      00007670
DXCONE(J)=0.0      00007680
DXCONE(J)=0.0      00007690
DXCONE(J)=0.0      00007700
DXCONE(J)=0.0      00007710
DXCONE(J)=0.0      00007720
NZNUCL(J)/10000      00007730
IF(NZ,ER,38,0R,-Z,ER,54) GO TO 30      00007740
DXCONE(J)=PCONE(J)*CNA      00007750
DXCONE(J)=PCONE(J)*EDA      00007760
DXCONE(J)=PCONE(J)*DWA      00007770
DXCONE(J)=PCONE(J)*DYE2      00007780
IF(TYPE,EQ,BAR) DXCONE(J)=PCONE(J)*EMA      00007790
IF(TYPE,EQ,BAR) GO TO 30      00007800
DXCONE(J)=SCON(J)      00007810
DFCVCS=1.0      00007820
IF(NZ,ER,1)DFCVCS=1.0      00007830
IF(NZ,ER,37,0R,-Z,ER,55) DFCVCS=2.      00007840
DXCONE(J)=DXCONE(J)/DFCVCS      00007850
CONTINUE      00007860
C      CALCULATE RADIODACTIVITY AFTER COLLECTION AT A CONSTANT RATE      00007870
C      CALL COLLECT(TC*86400.,DXCONE,ILITE,ITOT)      00007880
CALL COLLECT(TE*86400.,DXCONE,ILITE,ITOT)      00007890
CALL COLLECT(TD*86400.,DXCONE,ILITE,ITOT)      00007900
CALL COLLECT(T2*86400.,DXCONE2,ILITE,ITOT)      00007910
CALL COLLECT(TCH*86400.,DXCONE,ILITE,ITOT)      00007920
CALL COLLECT(TG*86400.,DXCONE,ILITE,ITOT)      00007930
CALL COLLECT(TRG*86400.,DXCONE,ILITE,ITOT)      00007940
40     IF(REGENT,LE,0.0) GO TO 50      00007950
CALL STORAGE(TRG*86400.,RINV,ILITE,ITOT)      00007960

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50 DO 100 I=1,ITOT
NZNUCL(I)=10000
TURBDR(I)=1991.*5.*SCON(I)
IF(NZ,EG,1) GO TO 100
IF(NZ,EG,55,DR,-Z,EG,55) GO TO 80
IF(NZ,EG,37,DR,-Z,EG,55) GO TO 70

CHEMICAL TREATMENT FOR OTHER CATIONS

CHCONE(I)=CHCONE(I)/DFC4
EDCONE(I)=EDCONE(I)/DFC4D
DHCONC(I)=DHCONC(I)/DFC4A
DHCON2(I)=DHCON2(I)/DFC4B
CHCONE(I)=CHCONE(I)*(1.0-BDTFR*(1.0-CHF4/DFC4))
TO TREAT PHA TURBINE BUILDING FLOOR DRAINS THROUGH DIRTY WASTE
SYSTEM, DELETE C FOR COMMENT ON CARDS RELATING UNTIL NEXT MESSAGE
RINV (I)=RINV (I)/DFRG
TURBDR(I)=1991.*5.*SCON(I)*PREF
TURBDR(I)=1991.*5.*SCON(I)*PREF/DFC4
GO TO 100

CHEMICAL TREATMENT FOR ANIONS

60 CHCONE(I)=CHCONE(I)/DFC1C
EDCONE(I)=EDCONE(I)/DFC1D
DHCONC(I)=DHCONC(I)/DFC1A
DHCON2(I)=DHCON2(I)/DFC1B
CHCONE(I)=CHCONE(I)*(1.0-BDTFR*(1.0-CHF4/DFC1C))
RINV (I)=RINV (I)/DF1RG
TURBDR(I)=1991.*5.*SCON(I)*HEF
TURBDR(I)=1991.*5.*SCON(I)*HEF/DFC1A
GO TO 100

CHEMICAL TREATMENT FOR PH AND CS

70 CHCONE(I)=CHCONE(I)/DFCSA
EDCONE(I)=EDCONE(I)/DFCSB
DHCONC(I)=DHCONC(I)/DFCSA
DHCON2(I)=DHCON2(I)/DFCSB
CHCONE(I)=CHCONE(I)*(1.0-BDTFR*(1.0-CHF4/DFCSH))
RINV (I)=RINV (I)/DFCSRG
TURBDR(I)=1991.*5.*SCON(I)*PREF
TURBDR(I)=1991.*5.*SCON(I)*PREF/DFCSA
100 CONTINUE

COMPUTE RADIODACTIVE DECAY DURING PROCESSING AND SAMPLING

CALL STORAG(TSTORH*88400.,CHCONE,ILITE,ITOT)
CALL STORAG(TS *88400.,EDCONE,ILITE,ITOT)
CALL STORAG(TSTORH*88400.,DHCONC,ILITE,ITOT)
CALL STORAG(TSTOR2*88400.,DHCON2,ILITE,ITOT)
CALL STORAG(TSTORH*88400.,CHCONE,ILITE,ITOT)
CALL STORAG(TSTORH*88400.,RINV,ILITE,ITOT)
CALL STORAG(21600.,TURBDR,ILITE,ITOT)
DO 130 I=1,ITOT
NZNUCL(I)=10000
ABLTHD=0.0
IF(REGENT,LT,0.001) GO TO 110
ABLTHD=RINV(I)*365.5*RGFD/REGENT
110 IF(TYPE,ED,BAR) GO TO 120
ABLTHD=ABLTHD+BLHDHN*1991.*CHCONE(I)*T1.*REFNRT

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GO TO 130
 120 ARBLW=ARBLW+CHFR*1.382*CHC(1)
 130 CHC(1)=ARBLW
 IF(TYPE, EQ, BWR) GO TO 133
 CHFR=8HLDRC*FD*0.02832
 EDFLR=EDFLR*EDFD*0.02832
 DXFR=DXFLR*DxFD*0.02832
 DXFR2=DxFLR2*DxF2*0.02832
 TPLRP=CHFR*CHA+EDFLR*EDA+DXFR*DXFA+DXFR2*Dx2
 H3RLPK=TPLRP*H3CPK
 IF(H3RLPK, GT, 0.5*H3PRP) H3RLPK=0.5*H3PRP
 RH3RLP=RH3RLP/10.
 INTRI=RH3RLP
 IH3RLP=INTRIM*10
 GO TO 136
 133 CHFR=CHFLR*1.382*CHFD
 DXFR=DxFLR*DxFD*1.382
 TLR=(CHFR*DxFR)*1.382*(CHFD*CHFR+RGFD*RGFR)
 TRITRL=TRITCD*TLR
 IF(TRITRL, GT, 0.5*TRITPR) TRITRL=0.5*TRITPR
 RTRITR=TRITRL*0.5
 ITRITR=RTTRITR
 136 TOTAL=0.0
 DO 140 I=1,ITOT
 NZ=NUCL(I)/10000
 IF(NZ, EQ, 36, DR, NZ, 54) GO TO 140
 DISI=DIS(I)*1.5*3E13
 CHC(1)=DISI*(CHC(1)*CHFR+EDC(1)*EDFLR)
 DC(1)=(CHC(1)*DXFR+DC(1)*DXFR2)*DISI
 CHC(1)=CHC(1)*DISI
 TURBDR(I)=TURBDR(I)*DTST
 IF(NUCL(I), EQ, 10030) GO TO 140
 TOTAL =TOTAL +CHC(1)+DC(1)+CHC(1)+TURBDR(I)
 140 CONTINUE
 ADI=0.15
 ADR=(ADI+TOTAL)/TOTAL
 150 SCNDRH=0.0
 SAPRIM=0.0
 SSEC=0.0
 SWAST=0.0
 SDWAST=0.0
 SARLDR=0.0
 STB=0.0
 STOTAL =0.0
 SCANAL=0.0
 SPER=0.0
 PAPRIM=0.0
 PSSEC=0.0
 PCWAST=0.0
 PDWAST=0.0
 PARLW=0.0
 PTB=0.0
 PTOTAL =0.0
 PCANAL=0.0
 PPER=0.0
 PNORMD=0.0
 TLAUND=0.0
 CTOTAL=0.0
 PRINT 9001, REACTR
 IF(TYPE, EQ, PWR) PRINT 9002
 IF(TYPE, EQ, BWR) PRINT 9006

00008580
 00008590
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 00009160
 00009170
 00009180

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PRINT QUIT
KOUNTR1
1MILITE*IACT+1
L81
DO 180 1M1,1TOT
1P(1,EG,1) PRINT 3011
NZ=NUCL(1)/1000
1P(NZ,EG,16,0,0,NZ,EG,54) GO TO 180
1P(NZ,EG,1) GO TO 180
DISIMDIS((1)*1.6283E+13
APRIMAPC(DC1)*D181
ASEC0,0
1P(TYPE,EG,PHR) ASEC=SEC(1)*0.01
CHASTE=CHCNC(1)
DHASTE=DHCNC(1)
ABLOW=HCHCNC(1)
TB=TURBORG(1)
TOTAL=CHASTE+DHASTE+ABLOW+TB
TOTALN=TOTAL*AO
NUCLINUCL(1)
XLAND=0.0
TOTALG=TOTALN
IN(NUCL,NE,LAUNDRY(L)) GO TO 155
XLAND=XLAND*(L)*PLAUN
TOTALG=TOTALN*XLAND*(L)*PLAUN
LBL+1
155 CONTINUE
1P(TOTALG,LT,1E-5) GO TO 156
1SUB#2
1P(1,EG,1,I)1SUB#1
DIV=10.*MCINT(CALCG10(TOTALG))-I1SUB#
TOTALG=MINT(TOTALG/DIV+0.5)*DIV
156 CONTINUE
1P(NUCL(1),EQ,1030) TOTALN=TOTAL
CANAL=TOTAL/DILUT*35.318
PERCENT=CANAL/MHC(1)*100.
1P(NZ,EG,1) GO TO 160
SAPRIM=SAPRIM+APRIM
SEC=SEC+SEC
ABLOW=ABLOW+ABLOW
SWAST=SWAST+CHASTE
SWAST=SWAST+DHASTE
STRETB+TB
STOTALE=STOTAL+TOTAL
SCANAL=SCANAL+CANAL
SPER=SPER+PERCENT
SNORM=SNORM+TOTALN
XLAND=XLAND+XLAND
CTOTAL=CTOTAL+TOTALG
160 1P(TOTALG,LT,1.E-5) GO TO 160
1P(MOD(KOUNTR,50),NE,0) GO TO 170
PRINT 9000, REACTR
1P(TYPE,EG,PHR) PRINT 9002
1P(TYPE,EG,BHR) PRINT 9006
170 CALL NOAH(NUCL(1),NAME)
THALW=0.025E-6/DIS(1)
1P(TYPE,EG,PHR) PRINT 9003, NAME, THALW, APRIM, SEC, CHASTE, DHASTE, DMASTE=0.0009750
1P(TYPE,EG,PHR) PRINT 9007, NAME, THALW, APRIM, CHASTE, DHASTE,
1 KOUNT=RKOUNTR+1

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IF(NZ,EG,1) GO TO 180
PAPRIM=PAPRIM+APRIM
PSSEC=PSSEC+ASEC
PCCAST=PCCAST+CAASTF
PDCAST=PDCAST+CAASTF
PAHLOX=PAHLOX+AHLOX
PTH=PTH+TH
PTOTAL=PTOTAL+TOTAL
PCANALE=PCANAL+CANAL
PPER=PUPER+PERCENT
PNORM=PNORM+TOTALN
180 CONTINUE
PAPRIM=SAPRIM+PAPRIM
PSSEC=SSEC+PSSEC
PCCAST=SCCAST+PCCAST
PDCAST=SDCAST+PDCAST
PAHLOX=SABLOX+PAHLOX
PTH=STRPTH
PTOTAL=STOTAL+PTOTAL
PCANAL=SCANAL+PCANAL
PPER=SPER+PPER
PNORM=SCNORM+PNORM
ISURE#2
IF (CTOTAL.GT.1.0)ISU#1
DIV#10,*((INT(ALOG10(CTOTAL))-ISURE))
CTOTAL=INT(CTOTAL/DIV*0.5)*DIV
IF (PNORM.LT.1E-51 GO TO 184
DIV#10,*((INT(ALOG10(PNORM))-2))
PNORM=INT(PNORM/DIV*0.5)*DIV
GO TO 186
343 184 PNORM=PNORM
186 CONTINUE
IF(TYPE.EQ.BWR) GO TO 190
PRINT 9004, PAPRIM, PSSEC, PCCAST, PDCAST, PAHLOX, PTH, PTOTAL, PNORM,
1 PNORM
1 PRINT 9005, SAPRIM, SSFC, SCCAST, SDCAST, SAHLOX, STH, STOTAL, SCNORM,
1 SCNORM, CTOTAL
1 PRINT 9012, IH3HLF
RETURN
190 PRINT 9008, PAPRIM, PCCAST, PDCAST, PAHLOX, PTOTAL, PNORM, PNORMT
PRINT 9009, SAPRIM, SCCAST, SDCAST, SAHLOX, STOTAL, SCNORM, TLAIND,
1 CTOTAL
195 PRINT 9012, ITRITR
RETURN
9000 FORMAT(1H1,20X,7A4,' LIQUID EFFLUENTS (CONTINUED)')
9001 FORMAT(1H1,20X,7A4,' LIQUID EFFLUENTS')
9002 FORMAT(1H0,55X,'ANNUAL RELEASES TO DISCHARGE CANAL')/20X,'COOLANT' C00010260
10CONCENTRATION$1.57(1#),1 ADJUSTED DETERGENT TOTAL 1/1 NUCLIDE C00010270
2E HALF-LIFE PRIMARY SECONDARY ADRIN RS MSC, ASTES SEC00010280
3DARY TURB BLDG TOTAL LBS TOTAL ASTES 1/10X, C00010290
4T(DAYS) 1E10(MICRO CT/M#),1X,4(COURTESY) 1,1(CURIES) 1X, C00010300
5I (CI/YR) (CI/YR) C00010310
9003 FORMAT(1X,A2,13,A1,2X,1PE9.2,2(2X,E9.2,2X),5(1X,0PF9.5,1X),2(1X,0PF0010320
1 F9.5,1X),0PF10.51 C00010330
9004 FORMAT(1X,1A11,1THRS$,1X,1PE9.2,4X,E9.2,2X,5(1X,0PF9.5,1X),
1 1X,0PF9.5,1X,0PF10.5) C00010340
9005 FORMAT(1 TOTAL 1/1 (EXCEPT THITIUM) 1,1PE9.2,4X,E9.2,2X,
1 5(1X,0PF9.5,1X),2(1X,0PF9.5,1X),0PF10.5) C00010350
9006 FORMAT(1H0,17X,'CONCENTRATION ANNUAL RELEASES TO DISCHARGE CANAL C00010380
1A1/1HX,T IN PRIMARY 1.43(1#),1 ADJUSTED DETERGENT TOTAL C00010390
2 1/1 NUCLIDE HALF-LIFE COOLANT HIGH PURITY LDX PURITY CHEMICA00010400

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3L TOTAL LBS      TOTAL      WASTES      />10X,? (DAYS)  MICRO C00010410
G1/HML)?,3E? ((CURIES)) , ? ((CURIES)) ((CI/YR)) ((CI/YR)) ((CI/YR))
5R1??
9007 FORMAT(1X,A2,I3,A1,2X,1PE9.2, 2X,E9.2,2X ,4(1X,0PF9.5,1X),2(1X,0P00010440
1F9.5,1X),1X,0PF9.5)
9008 FORMAT(1X,'ALL OTHERS',9X,1PE9.2,2X,4(1X,0PF9.5,1X),1X,0PF9.5,4X, 00010460
1 10.0?,6X,0PF9.5) 00010470
9009 FORMAT(' TOTAL',1?,? (EXCEPT TRITIUM) 1,1PE9.2,2X,4(1X,0PF9.5,1X),00010480
1 2(1X,0PF9.5,1X,0PF9.5) 00010490
9010 FORMAT(' CORROSION AND ACTIVATION PRODUCTS') 00010500
9011 FORMAT('DEFISSION PRODUCTS') 00010510
9012 FORMAT(1H0,1X,'TRITIUM RELEASE',12X,13,? CURIES PER YEAR) 00010520
END
BLOCK DATA
COMMON /CONV/RCONE(800),SCUTV(800),SCUTP(800),SCOT(800)
COMMON /COMP/P=CNCC(800)
DATA RCONE/36*0,9E-3,13*0,2E-4,53*0,5E-3,4*1.6E-5,0.0,5E-2,3*0,
11F=3,3*0,3E-5,0.0,2F=4,2*0,4E-4,7*0,1E-6,0.0,3F=4,2*0,3E-2,4*0,
22E=4,3*0,2E-3,9E=0,3E=4,64*0,7E=3,63*0,3E=3,4*0,5E-3,2*0,3F=3,
319*0,5E=3,1E=4,3*0,6E=6,5*0,4E=5,5*0,1E=2,6E=3,4*0,4E=3,
411*0,7E=6,0.0,7E=6,6*0,5E=6,5*0,4E=3,2*0,2E=3,2F=2,8E=0,9E=2,7*0,
52E=5,3*0,8E=2,6*0,2E=3,4*0,3F=6,21*0,1F=h,104*0,4F=5,13*0,1F=4,
60,0,5E=3,5*0,1E=5,3E=2,4*0,2E=2,5*0,7E=2,2*0,3E=5,2*0,2E=2,8*0,
72E=5,3*0,7F=5,4*0,1E=2,4*0,1E=2,3*0,4E=4,4*0,1E=2,2,0,0,3E=5,5*0,
8E=3,5E=3,7*0,3E=5,4E=5,5*0,2*0,3E=6,10*0,3E=6,81*0/
DATA P=CNCC/104*0,1,9E-3,4*0,5,1E=4,5*0,1,6E=3,3*0,1E=3,0,0,0,018,
12*0,2E=3,185*0,1,2E=3,65*0,4,8E=3,4*0,2,6E=5,2*0,3F=4,8*0,8,5E=5,
28*0,,2,440,3,5E=4,3*0,1E=5,0,0,1,2E=6,3*0,6,5E=4,3,8F=4,8,4E=5,9*00010680
3,3,4F=5,11*0,6E=5,0,,5F=5,15*0,,084,,048,16*0,4,5F=5,4,5E=5,14*0,, 00010690
41E=5,0,0,1E=5,103*0,2,4E=5,8*0,2,8E=4,8,5E=4,10*0,1,4E=3,1,6E=3,, 00010700
58*0,2,1E=3,3*0,2,5E=3,1,1E=3,,27,5*0,,027,,1,4*0,2,38,5*0,,047,2*0,00010710
6,025,2*0,,19,8*0,,013,3*0,,018,,016,12*0,2,2E=4,1,5E=4,5*0,7E=5,
712*0,4E=5,5E=5,2*0,3,3E=5,5,3F=5,91*0/ 00010730
DATA SCUTV/104*0,9E=8,4*0,2F=8,5*0,HE=R,3*0,6F=8,0,0,0,8F=7,2*0,
19E=8,185*0,6E=8,63*0,h,9F=8,4*0,1,5E=8,2*0,2E=10,6*0,4,4E=9,8*0,, 00010750
27,4E=7,4*0,2E=8,3*0,0,4F=10,0,0,0,8F=11,3*0,2F=8,1F=R,3E=9,9*0,1E=9,
311*0,4E=9,0,0,0,4F=9,15*0,4E=6,3E=6,16*0,2E=9,2E=9,14*0,4E=10,0,0,, 00010770
44E=10,103*0,1E=09,8*0,0,1E=R,3F=8,10*0,6E=R,6E=8,8*0,0,4,8F=8,3*0,, 00010780
51E=7,2E=8,6,8*0,6,5*0,1E=0,1,9E=6,4*0,0,8,9F=6,5*0,3,8E=7,2*0,1,5F=6,00010790
62*0,3,8E=6,8*0,6,7E=7,3*0,9,4E=7,9E=7,12*0,1E=8,7E=9,5*0,4E=9,, 00010800
712*0,1E=09,2E=9,2*0,2F=9,2F=9,91*0/ 00010810
DATA SCUTP/104*0,9E=7,4*0,0,2E=7,5*1,7E=7,3*0,5E=7,0,0,7E=6,2*0,
19E=7,185*0,3E=7,63*0,1,5E=7,4*0,2E=8,2*0,2E=10,6*0,4E=8,8*0,8E=7,, 00010830
24*0,2E=7,3*0,5E=9,0,0,2E=9,3*0,8E=8,3F=8,3E=8,8*0,9E=9,11*0,3E=8, 00010840
30,0,3E=8,15*0,0,3,0E=5,3,0E=5,16*0,2E=8,2E=8,14*0,5E=9,0,0,5E=9,, 00010850
4103*0,9E=9,8*0,9F=8,2E=7,10*0,6E=7,6E=7,8*0,2,5F=7,3*0,5E=7,5E=7,, 00010860
51,1E=4,5*0,8E=6,1,1E=5,4*0,6,5E=5,5*0,5,7E=7,2*0,1,2E=5,2*0,, 00010870
61,4E=5,8*0,5E=6,3*0,8E=6,8E=6,12*0,9E=R,8E=8,5*0,3E=8,12*0,9E=9,, 00010880
72E=8,2*0,2E=8,2E=8,91*0/ 00010890
DATA SCUT/104*0,9E=10,4*0,0,2E=10,5*0,8E=10,0,0,8E=9,2*0,, 00010900
19E=10,185*0,6E=10,63*0,2,3E=9,0*0,1,2E=9,2*0,,0E=10,6*0,7E=11,8*000010910
2,2,E=7,4*0,2E=10,3*0,5F=12,0,0,8F=13,5*0,3E=10,2E=10,3E=11,9*0,, 00010920
32E=11,11*0,3E=11,0,0,2E=11,15*0,4F=7,2E=7,16*0,2E=11,2F=11,14*0,, 00010930
45E=12,0,0,5E=12,103*0,1F=11,8*0,1E=10,4E=10,10*0,7E=10,8E=0,, 00010940
51E=9,3*0,0,5F=10,5E=10,1,3F=7,5*0,1E=8,4,7E=8,4*0,1,8E=7,5*0,2,2E=8,00010950
62*0,2,0E=8,2*0,9,0E=8,8*0,1,0E=8,3*0,1,5E=8,8E=9,12*0,1E=10,7E=11,00010960
75*0,3E=11,12*0,2E=11,2F=11,2*0,2E=11,2F=11,91*0/ 00010970
END
SUBROUTINE SOLVE
COMMON/EQ/XZERO(800), XZH(800), XTEMP(800), XNE=(10,800),
1  R(800),DE(800) 00010980
00010990
00011000
00011010

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COMMON/FLEX/FLUX(110),NNN,NOUT,INDEX,OXX,ANX,ERR,NORLN,"ZERO"
COMMON/PRCSS/  WPROS,PRATE(H),NPROMS(H),TPRMS(8,20),PH(80)
COMMON/FLUXN/ T(20),PWR(10),TOCAP(800),F18(100),DIS(Bnn),LTTE,
  IFACT,ISPT,ITOT,NN,NINT
COMMON/DUT/NUCL(100),TITLE(20),W(HN0),FG(100),CUTOF(7),
  I POW,HURNUP,FLUR,STAR,ALPHANT(100),SPONT(100),ARUND(500),
  2 BASIS(10),TCNST,TUNIT
  D(T)•DIS(1)
  10 XTEMP(1)=0.0
  DELT=T(1)*TCNST
  CALL DECAV(1,DELT,ITOT)
  CALL TERM(CDELT,LTTE,ITOT)
  CALL EQUI(1,ITOT)
D/ 30 IM1,ITOT
  XTEMP(1)=XNEW(1)
  RETURN
END
SUBROUTINE TERM(1,M,LTTE,ITOT)
  C
  C TERM ADDS ONE TERM TO EACH ELEMENT OF THE SOLUTION VECTOR
  C CSUM(J) IS THE CURRENT APPROXIMATION TO XNEUT(M,J)
  C CIW(J) IS THE VECTOR CONTAINING THE LAST TERM ADDED TO EACH
  C ELEMENT OF CSUM(J)
  C CMN(J) IS THE VECTOR CONTAINING 1/TUN TIMES THE NEW TERM TO BE
  C ADDED TO CSUM(J)
  C CSUM(J) IS GENERATED FROM CIW(J) BY A RECURSIVE RELATION
  C CIW(J) IS SUM OVER L OF (AP(L,J)*CIW(L))
  C AP(L,J) IS THE REDUCED TRANSITION MATRIX FOR THE LONG-LIVED
  C NUCLIDES
  C
  LOGICAL L
  INTEGER*2 LOC,ND,ND
  INTEGER*2 LINCP(2500)
  INTEGER*2 NNDP(800)
  INTEGER*2 HQ,NGU,QUEUE
  REAL*8 RATE,BATV
  REAL*8 CIW(800),CSUM(800),CIW1
  DIMENSION AP(2500),CIW(800),CIW0(800)
  DIMENSION QUR(50)
  COMMON/SERIES/ XP(800),XPAH(800),LUNG(800)
  COMMON/FLEX/FLUX(110),NN,NOUT,INDEX,OXX,ANX,ERR,NORLN,"ZERO"
  COMMON/EGYZE/ZN(800),XZH(800),XTEP(800),XEW(10,800),
  H(800),DR(800)
  COMMON/MATRIX/AL(2500),LNC(2500),ND(4000),WD(800)
  COMMON/DEBBUG/AP
  COMMON/TERM/DT(100),EXP(100),QUEU(50),NQU(50),NQUEU(50),
  NUD(50)
  NNN
FIRST CONSTRUCT REDUCED TRANSITION MATRIX FOR LONG-LIVED ISOTOPES
  DO 220 L=1,ITOT
  I=(NU+L)*NU
  NUM=NU*NU
  TP(H,GT,NN,0.0,EQ,MRHL)  NUMEQ(1)
  CIWAC(L)=AL(L)
  IF(NUMLE,NUL) GM(T)=210
  NGU=N+1
  NNUJL
  NNUJM=NUJL
  DJ 200 NNUJ,L
  NNN+1

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JED0CTN

AC011630

DD011630

C THIS IS A TEST TO SEE IF THE ASSYMPTOTIC SOLUTIONS APPLY FOR THE
C EQUILIBRIUM CHAIN WHICH IS NOT IN
C GOING BACK UP THE CHAIN, TO FIND A PARENT WHICH IS NOT IN
C EQUALTHWICH
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      DO 100 K=1,T1
      XPL=EXP(XPL)
      IF(XPL*XPL,LT,ERR) GO TO 100
      DX=DD(XK)
      PRD=DL/DK=1.0
      DK=PRD
      IF( ABS(PRD),GT,1.E-4) GO TO 80
      C USE THIS FORM FOR TWO NEARLY EQUAL HALF-LIVES
      PRD=DX*XPL*(1.0E-5*(DL-DK)*T)
      GO TO 70
  60  PRD=(XPL-XPL)/PRD
      PRD1=XPL/DK
      70  PT=1.0
      S1=2./DK*T
      DO 90 JK=1,II
      IF(JK,LT,KB) GO TO 90
      S=1.0-DK/DD(JK)
      IF( ABS(S),GT,1.E-4) GO TO 80
      IF(ABS(DK),GT,1.E-4) PRD=PRD1
      S=S1
      80  PT=PT*S
      IF(AHSCPT),GT,1.E25) GO TO 100
      90  CONTINUE
      RATE=BATE+PRD1/PT
      100 CONTINUE
      C IF SUMMATION IS NEGATIVE, SET EQUAL TO ZERO AND PRINT MESSAGE
      IF(RATE,LT,0.000) PRINT 9001, L,IM,RATE,BATH
      9001 FORMAT('1RATE IS NEGATIVE IN TERM, THERE ARE MORE THAN TWO SHORT-LIVED NUCLIDES IN A CHAIN WITH NEARLY EQUAL DIAGONAL ELEMENTS',I7,I10)
      21 L,IM,RATE,BATH = 1,215,1P2E12.5)
      IF(RATE,LT,0.000) RATE=0.00
      BATH=BATH+RATE
      110 CONTINUE
      DRA=AKDJN*AMAX1(DRR,0.0)*DJ
      GO TO 130
  120 DRA=AKDJN*AMAX1(DRR,0.0)*DJ
      130 IF(NB,GT,NN) GO TO 150
      DO 140 LJ=NNS,NN
      IF(LDCP(LJ),NE,J1) GO TO 140
      AP(LJ)=AP(LJ)+DRA
      GO TO 180
  140 CONTINUE
  150 NSAVE=N
      AP(NN)=DRA
      LDCP(NN)=J1
      GO TO 180
  160 IF(AKDJN,LE,1.0E-06) GO TO 180
      IF(NSAVE,GE,50) GO TO 180
  170 NSAVE=NSAVE+1
      NQUEUE(NSAVE)=J1
      QUEUE(NSAVE)=AKDJN
      NQUEUE(NSAVE)=J
      QUEUE(NSAVE)=DRR=1./D(J*T)
      180 CONTINUE
  190 IF(NSAVE,LE,0) GO TO 200
      J=NQUEUE(NSAVE)
      QUEUE=QUEUE(NSAVE)
      NG(J)=NQU(NSAVE)
      DRR=QUR(NSAVE)
      CIMA(L)=CIMA(L)+QUEUE(H(J))*AMAX1(DRR,0.0)
      NSAVE=NSAVE-1

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GO TO 20
200 CONTINUE
210 NUM=0.0(L)
220 CONTINUE
C FIND NORM OF MATRIX AND ESTIMATE ERROR AS DESCRIBED IN LAPLUS
C AND LUUS, OPTIMAL CONTROL OF ENGINEERING PROCESSES HLAISNET, 1987
C FIND THE MINIMUM OF THE MAXIMUM ROW SUM AND THE MAXIMUM COLUMN SUM
C ASUM =0.0
ASUM=0.0
NULL:
DO 250 I=1,ITOT
IF(.NOT.LONG(I)) GO TO 250
DIM=D(I)*T
AJ=DT
AJ=DT
N=LNCP(I)
IF(NUL.GT.NUM) GO TO 240
DO 230 A=NULL,NUM
230 AJ=A+AP(N)
240 AJ=DI
IF(DI.GT.ASUM) ASUM=AJ
IF(AJ.GT.ASUM) ASUM=AJ
N=LNCNP(I)+1
250 IF(ASUM.LT.ASUM) ASUM=ASUM
C USE ASUM TO DECIDE HOW MANY TERMS ARE REQUIRED AND ESTIMATE ERROR
C NLARGE=3.5*ASUM+.5.
NLARGE=XLARGE
XLARGE=EXP(ASUM)*(ASUM**2.71828/XLARGE)**NLARGE/SQRT(.2832*XLARGE) 0001311
ERR=EXP(ASUM)*PRINT 9002,ERR,ASUM,NLARGE
9002 FORMAT(1X,1X,1X,F3.0,1X,F10.6),TRACE# F10.4,
1 NLARGE# 'b'
C NEXT GENERATE MATRIX EXPONENTIAL SOLUTION
DO 260 I=1,ITOT
C=UM(I)*XTMP(I)
C=M(I)*XTMP(I)
260 CONTINUE
ERRQ=0.01ERR
DO 310 K=1,NLARGE
DO 270 I=1,ITOT
C=M(I)*CINH(I)
270 CONTINUE
T=UNSTAY
NULL:
DO 300 I=1,ITOT
IF(.NOT.LONG(I)) GO TO 300
NUM=LNCP(I)
CINH=0.0
IF(NLT.EQ.1) CINH=CINH(I)
IF(NUL.GT.NUM) GO TO 290
DO 280 M=NULL,NUM
J=LNCP(N)
280 CINH=CINH(I)*AP(N)*CINH(J)
290 CINH=CINH(N+0(I))*CINH(I)
CINH=T*CINH(I)
IF(DABS(CINH)=LT.ERR3) CINH=0.0
CINH=CINH(I)*CINH(I)
CINH=CINH(I)*CINH(I)+CINH(I)
300 NULL=LNCP(I)+1
CONTINUE
310 CONTINUE
DO 320 I=1,ITOT
IF(CSUM(I).LT.ERR) CSUM(I)=0.0

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320  CONTINUE
      RETURN
END
C   SUBROUTINE DECAY(T,TTOT)
C   DEACY TREATS SHORT-LIVED ISOTOPES AT HEATING OF CHAINS USING
C   BITEMAN EQUATIONS
C   LOGICAL= LONG
REAL*8 DATE
INTEGER*2 L1C,INDX,K
COMMON/DEHIGG/AP(500)
COMMON/SERIES/XP(800),XPAR(800),LUNG(800)
COMMON/DELUX/LUX10,I,M,N,ROUT,INDEX,DXN,AN,ERR,NBLND,NZERO
COMMON/EGZER/EGZER(800),XZ(800),XEW,P(H001)XNE(10,800),
H(800),D(800)
COMMON/MATRIX/AC(500),LNC(2500),NUV(800),NUD(800)
COMMON/TEMD/DT(100),EXP(100),QUE(50),QUV(50),NUQUE(50),NU(800)
DO 10 I=1,TTOT
  XPAR(I)=0.0
  LONG(I)=FALSE,
  XPI=0.0
  DT=DT-LT*50.0, GO TO 10
  IF(ABS(DT),LE.,AN) LONG(I)=.TRUE.
  XPI=EXP(DT)
  10 XP(I)=XPI
  NUL=1
  DO 160 L=1,LT
    XTE=0.0
    DL=DL(L)
    NUM=NUM(L)
    NUX=NUX(L)
    IF(.GT..MIN(.IR,.EQ..ZERO)) NUX=0.0
    IF(NUM,LT,NUL) GO TO 150
    DO 140 N=NUL,NIN
      JALC(N)
      LJ=L(J)
      IF(LNG(LJ)) GO TO 140
      C  USE THIS FORM FOR TWO NEARLY EQUAL HALF-LIVES
      IF(ABS(DL/DJ)=1.0).LE.1.0E-5) XTE=XTEM*XTEMP(J)*A(N)*XP(J)*T
      IF(ABS(DL/DJ)=1.0).GT.1.0E-5)
      1 XTE=XTEM*XTEM(J)*(XP(J)*A(N)*(XP(L)/XP(DJ))/(DL-DJ))
      GIE=A(N)/D
      N2(L)=0
      N0(J)=0
      NSAVE=0
      20 NUX=NNU((J))
      IF(.GT..NNU,.OR..NE..ZERO)) NUX=0.0
      NUF=1
      IF(J,GT,1) NUF=NNU(J-1)+1
      IF(.NE..GT,AUX) GO TO 130
      DO 120 K=NUF,NUX
      JALC(K)
      IF(LNG(J)) GO TO 120
      XPI
      30 IF(J1,EQ,NG(KP)) GO TO 120
      K=NQ(KP)
      IF(KP,NE,0) GO TO 30
      DIB=D(J1)
      AKD=AK(J1)/D*GIE
      IF(AND(J1,LE,1,0F000)) GO TO 120
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N0(11)46
101
K0EJY
0.0
DPRINT(XP(L))
K0EJY(XP)
102 XE(L,0) GO TO 50
103 I=1
104 IF(I.LE.100) GO TO 40
PRINT 9000, W1,L,J1,J2,A(1,3)
9000 FORMAT(1I11,1I5,1I2,5)
GO TO 130
105 RATE=0.0
106 T1=1
107 XPL=XPL(L)
C D R VINDY FROM OF RATHMAN EQUATIONS == GRANDE=501
108 D1=0.0#1#1#1
109 XPL=XPL(L,EHR) GO TO 100
110 T=XP(L+XP(L,L,EHR)) GO TO 100
111 D=XP(L,EHR)
112 PRINT(D1/DK=1.0)
113 D#R#R#D
114 T=(A#S#P#C#O),GT,1.E-42 GO TO 60
115 PRINT*D#X#P#J={1,0,0,5*(L#N#J#1)}
116 GO TO 70
117 P#ON#(XP#-XP#)/P#R#D
118 P#0#1#X#P#J#D#R
119 P#T#1#0
120 S1#2#/(OK#T)
121 GO TO JK#1#1
122 T#T(J#,E#J#,KH) GO TO 40
123 S#1#W#D#D#(JK#)
124 T#T(A#S#S#) GT,1.E-40 GO TO 80
125 USE THIS FORM FOR TWO NPAWLY EQUAL MATERIALIVES
126 T#T(A#S#OK#),GT,1.0E-40 PRINT#P#R#U
127 S=S1
128 P#P#P#S
129 T#T(A#P#),GT,1.E25) GO TO 100
130 RATE#HATE#PRO#P#T
131 CONTINUE
132 IF(HATE#LT.0.001 PRINT 901, L,T,HATE,XTEM,XTEM#P(J#1),OK#D#0
133 9001 FORWARD L,T,RATE,XTEM#P(J#1),AND#C=1,215,1P#E12.5)
134 IF(HATE#LT.0.001) HATE#D#0
135 XTEM#XTEM#P(J#1)*AND#D#0#HATE
136 T#T(SAVE,GF,S#1) GO TO 120
137 SAVE#SAVE+1
138 AND#D#C#SAVE#J#1
139 GO#E#(C#SAVE#) #AND#J#1
140 CONTINUE
141 120 IF(SAVE#LE.0) GO TO 140
142 J#NO#E#E#(SAVE)
143 Q#E#Q#E#E#(SAVE)
144 NO#J#J#N#U#(SAVE)
145 S#A#V#E#>SAVE#1
146 GO#E#(C#SAVE#) #AND#J#1
147 130 CONTINUE
148 130 IF(SAVE#LE.0) GO TO 140
149 J#NO#E#E#(SAVE)
150 Q#E#Q#E#E#(SAVE)
151 NO#J#J#N#U#(SAVE)
152 S#A#V#E#>SAVE#1
153 GO#E#(C#SAVE#) #AND#J#1
154 140 CONTINUE
155 140 IF(T#T(N#L#N#L#)+1 XTEM#(L#)XTEM#XTEM#P(L#)*XP(L#)
156 N#L#N#L#N#L#+1 XTEM#(L#)XTEM#(L#)XTEM#XTEM#P(L#)*XP(L#)
157 N#L#N#L#N#L#+1 XTEM#(L#)XTEM#(L#)XTEM#XTEM#P(L#)*XP(L#)
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165 N#L#N#L#N#L#+1 XTEM#(L#)XTEM#(L#)XTEM#XTEM#P(L#)*XP(L#)
166 N#L#N#L#N#L#+1 XTEM#(L#)XTEM#(L#)XTEM#XTEM#P(L#)*XP(L#)
167 N#L#N#L#N#L#+1 XTEM#(L#)XTEM#(L#)XTEM#XTEM#P(L#)*XP(L#)

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160 CONTINUE
D1 170 I=1,ITOT
IF(LONG(I)) XTEMP(I)=XTEMP(I)*XPAR(I)
IF(.NOT,LONG(I)) XTEMP(I)=0.0
170 CONTINUE
RETURN
END
SUBROUTINE EQUIL(X,ITOT)

C EQUIL PUTS SHORT-LIVED DAUGHTERS IN EQUILIBRIUM WITH PARENTS
C EQUIL USES GAUSS-SEIDEL ITERATION TO GENERATE STEADY STATE
C CONCENTRATIONS
C
LOGICAL*1 LONG
INTEGER*2 LOC,NODE,KD
COMMON/EG/XZERO(800),XZH(800),XTEMP(800),XNEW(10,800),
1 H(800),D(800)
COMMON/MATRIX/A(2500),LIC(2500),HOD(800),RD(800)
COMMON/FLEX/FLUX(10,MNN,MNU,T,INDX,XN,XN1,ERR,NBLND,MZERO)
COMMON/SERIES/ XPI(800),XPAR(800),LONG(800)
DO 10 I=1,ITOT
XPAR(I)=0.0
IF(.NOT,LONG(I)) GO TO 10
XTEMP(I)=XTEMP(I)*XPAR(I)
XPAR(I)=MAX1(XNEW(I),I)-XTEMP(I),0.0
10 CONTINUE
ITER=1
20 N=0
BTG=0.0
DO 80 I=1,ITOT
NUM=MNU(I)*N
DI=D(I)
IF(LONG(I)) GO TO 50
XNEW(I)
IF(M,GT,MNN,LT,M,EQ,MZERO) NUM=MNU(I)*N
IF(NOT,EQ,0) GO TO 31
DO 30 K=1,NUM
N=N+1
J=LOC(N)
D=DI(J)
X=X*PAR(J)
IF(LONG(J)) X=X*X+XTEMP(J)/(1.0-BJ/DI)
XNEW=XNEW+A(N)*X
30 CONTINUE
31 X=X*X/N/DI
IF(XNN,LT,1.0E-50) GO TO 40
ARG=ABS((XNN-XPAR(I))/XNN)
IF(ARG,GT,RIG) RIG=ARG
40 XPAR(I)=XNN
50 N=NOD(I)
60 CONTINUE
IF(HIG,LT,XNN) GOTO 70
ITER=ITER+1
IF(CITER,LT,1000) GO TO 20
PRINT 9000
STOP
70 DO 80 I=1,ITOT
IF(.NOT,LONG(I)) XNEW(M,I)=XNEW(M,I)+XPAR(I)
80 CONTINUE
RETURN
9000 FORMAT(' GAUSS SEIDEL ITERATION DID NOT CONVERGE IN EQUIL')

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END
SUBROUTINE NUDATA(NLIRE)
  NLIRE VERSION TO HANDLE THREE TYPES OF NUCLEAR DATA LIBRARIES
  HAS POINTER, NLIRE, = 1 FOR HTGR
  = 2 FOR LIGHT WATER REACTOR
  = 3 FOR LFRHR
  = 4 FOR HSRR
  INTEGER*2 LOC,NHND,KD
  INTEGER*2 FLE(99),STA(2)
  INTEGER*2 KAP(800),NMAX(800)
  INTEGER*2 NAME(3)
  DIMENSION COEFF(7,800),NPROD(7,800),CART(6),
  1 NUCAL(6),NSORG(5),          YIELD(5,800),TYLD(5)
  DIMENSION Y(5)
  DIMENSION SKIP(20)
  DIMENSION HSRS(20)
  COMMON/LABEL/ELF,STA
  COMMON/FLEX/FLUX(10),MN,MOUT,INDEX,QXN,AXN,ERR,NBLUND,MZERO
  COMMON/ENR/XZERO(800),XZH(800),XTEMP(800),XHE(10,800),
  1     H(800),D(800)
  COMMON/RPC/NPCTAB,ANRPC(800),NPDC(800)
  COMMON/FLUX/T0201,PRKER(100),T0CAP(800),FISS(100),D18(800),TLITE,
  1 IACT,IFF,ITOT,NON,INPT
  COMMON/ZOUT/NCOL(800),TITLE(20),Q(800),FG(800),CUTOFF(7),
  1 PTH,RURNUP,FLUXH,HSTAR,ALPHAN(100),SPINF(100),ABUND(500),
  2 RASTR(10),TCNST,TUNIT
  COMMON/MATRIX/A(2500),LOC(2500),NHND(800),KD(800)
  EQUIVALENCE (XZERO(1),KAP(1)),(XZERO(4011),NMAX(1)),
  1   (XZH(1),COEFF(1,1)),(XHE(1,4011),NPROD(1,1))
  EQUIVALENCE (A1,DIAH)
  DATA NUCAL/20030,10000,10,11,10,-9/
  DATA HSRS/922330,922350,902320,922380,942390,922330,922350,942410,00015600
  1   922380,942390,942410,922350,942400,922380,942390,922330,00015610
  2   922350,902320,922380,942390/
  PROGRAM TO COMPUTE A MATRIX (TRANSITION MATRIX) FROM NUCLEAR DATA 00015640
  READ 9011,      (TITLE(I),I#1,10),NLIRE 00015650
  IF(NLIRE.LT.0) PROGRAM WILL READ TAPE IN CASDAR FORMAT 00015660
  IGH=0
  IF(NLIRE.GT.0) GO TO 10 00015670
  IGH=1 00015680
  NLIRE=NLIRE 00015690
  PRINT 9000 00015700
  9000 FORMAT(1H0,1WILL READ TAPE GENERATED BY CASDAR!) 00015710
  10 NLIRE=NLIRE 00015720
  20 READ 9001,      THERM,RES,FAST,ERR,NMD,NDAY,NYR,NPCTAB,INPT,IR 00015730
  PRINT 9005,      NMD,NDAY,NYR 00015740
  PRINT 9006 00015750
  PRINT 9007 00015760
  PRINT 9008 00015770
  PRINT 9009 00015780
  PRINT 9010 00015790
  PRINT 9013 00015800
  PRINT 9014 00015810
  THERM = RATIO OF THERMAL FLUX TO TOTAL FLUX 00015820
  RES = RATIO OF RESONANCE FLUX TO TOTAL FLUX 00015830
  FAST = RATIO OF FAST FLUX TO TOTAL FLUX 00015840
  ERR = TRUNCATION ERROR LIMIT 00015850
  NMD = NUMBER OF MESH DIVISIONS 00015860
  NDAY = NUMBER OF DAYS 00015870
  NYR = NUMBER OF YEARS 00015880
  00015890

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C      READ DATA FOR LIGHT ELEMENTS          06015900
C
C      K=5*(NLIRE+1)                      06015910
C      DO 30 K1=1,5                      06015920
C      K2=K+1
C      30 NSIORS(K1)=M8RS(K2)           06015930
C      PRINT 9018,  THEWM,RES,FAST,(NSIORS(K1),K#1,5),NLIRE 06015940
C      I#0
C      NUTAPE#0                           06015950
C      I#I+1                           06015960
C      40 READ(B,9034,END=260)NUCL(I),DLAM,IU,FH1,FP,FP1,FT,FA,FSF, 06015970
C      1Q(I),FG(I),ABUND(I),AMPC(I),AMPC(I)
C      IF(EIGC,GT,0) GO TO 70          06015980
C      DO 60 N#1,NLIRE                  06015990
C      60 READ(B,9035) SIGTH,FG1,FNA,FNP,RITH,FINA,FINP,SIGHEV,FN2N1,FNA, 06016000
C      1      FFNP,IT                   06016010
C      GO TO 90                         06016020
C      70 DO 80 N#1,NLIRE                  06016030
C      80 READ(B,9040) SIGTH,FG1,FNA,FNP,RITH,FINA,FINP,SIGHEV,FN2N1,FNA, 06016040
C      1      FFNP,IT                   06016050
C      90 IF(N1,EQ,0) GO TO 110          06016060
C      DO 100 N#1,N1                     06016070
C      100 READ(B,9036) SKIP            06016080
C      110 IF(IT,EQ,0) GO TO 50          06016090
C      120 H#0
C      CALL HALF(A1,IU)                 06016100
C      NUCLI=NUCL(I)
C      IF(NUCL,I,ER,0) GO TO 260        06016110
C      CALL NUCL(NUCLI,NAME)            06016120
C      IF(MOD(I=1,50),EQ,0) PRINT 9012, (TITLE (N),N#1,18) 06016130
C      IF(MOD(I=1,50),EQ,0) PRINT 9018
C      SIGTH*THEWM*SIGTH
C      RITH*RES*RITH
C      SIGHEV*FAST*SIGHEV
C      SIGVA*SIGTH*FINA*RITH*FINA*SIGHEV*FFNA 06016140
C      SIGNP*SIGTH*FNP*RITH*FINP*SIGHEV*FFNP 06016150
C      FNGB1,0=FINA=FNP
C      IF(FNG,LT,1,DE=4)FNGB0,          06016160
C      FNGB1,0=FINA=FINP             06016170
C      IF(FNG,LT,1,DE=4)FNGB0,          06016180
C      FN2#1,0=FFNA=FFNP             06016190
C      IF(FN2N,LT,1,DE=4)FN2N0,          06016200
C      SIGNG*SIGTH*FNG*RITH*FNG
C      SIGN2#SIGHEV*FN2N             06016210
C      130 PRINT 9033, NAME,          06016220
C      1      DLAM,FH1,FP,FP1,FT,FA,SIGNG, 06016230
C      C      TEST RADIODACTIVITY          06016240
C
C      140 IF(A1,LE,ERR) GO TO 180        06016250
C      ARETA#1,0                         06016260
C
C      TEST POSITRON EMISSION          06016270
C
C      IF(FP ,LT, ERR) GO TO 150        06016280
C      M#4+1
C      COEFF(M,I)=FP*A1               06016290
C      KPROD(M,I)=NUCLI=10000          06016300
C      ARETA=ARETA*FP                  06016310
C
C      TEST POSITRON EMISSION TO EXCITED STATE OF PRODUCT NUCLIDE 06016320
C
C      150

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IF(FRT .LT. ERR) GO TO 150
H=M+1
CDEFF(M,I)=EFF1*CDEFF(M=1,I)
NPROD(M,T)=NPROD(M=1,T)+1
CDEFF(M=1,T)=CDEFF(M=1,I)*CDEFF(M,T)

C TEST ISOMERIC TRANSITION
C
150 IF(FT .LT. FRR) GO TO 160
H=M+1
CDEFF(M,T)=FT*A1
NPRUD(M,T)=NUCLT
ARETABA=BETAFT

C TEST ALPHA EMISSION
C
160 IF(FA .LT. ERR) GO TO 170
H=M+1
CDEFF(M,I)=FA*A1
NPRUD(M,I)=NUCLT+20040
H=M+1
CDEFF(M,I)=CDEFF(M=1,I)
NPROD(M,I)=20040
ARETABA=BETAFA

C TEST NEGATRON EMISSION
C
170 IF(BETA.LT.1,F=1) GO TO 180
H=M+1
CDEFF(M,T)=BETA*A1
NPRUD(M,T)=NUCLT+10000
C TEST NEGATRON EMISSION TO EXCITED STATE OF PRODUCT NUCLDE
C
IF(FRT .LT. ERR1) GO TO 180
H=M+1
CDEFF(M,I)=F11*CDEFF(M=1,I)
NPROD(M,I)=NPROD(M=1,I)+1
CDEFF(M=1,T)=CDEFF(M=1,I)*CDEFF(M,T)

C COMPUTE NEUTRON CAPTURE CROSS SECTIONS IN THREE REGIONS
C
180 KAP(T)=H
DO 190 K1=1,6
CAPT(K1)=0.0
CAPT(1)=SIGN4
CAPT(2)=SIGNP
CAPT(4)=SIGNG*PNG
CAPT(5)=SIGNG=CAPT(4)
CAPT(6)=SIGN2N*PN2N1
CAPT(8)=SIGN2N=CAPT(6)
TOCAP(I)=U_0
TOTAL NEUTRON CROSS SECTION FOR NUCLEIDE(I)
DO 220 K=1,8
CAPTK=CAPT(K)
IF(CAPTK.LT.ERR) GO TO 220
H=M+1
NPRUD(M,I)=NUCLT+NUCAL(K)
CDEFF(M,T)=CAPTK
TOCAP(I)=TOCAP(I)+CAPTK
IF(K,NE,1) GO TO 210
      00016510
      00016520
      00016530
      00016540
      00016550
      00016560
      00016570
      00016580
      00016590
      00016600
      00016610
      00016620
      00016630
      00016640
      00016650
      00016660
      00016670
      00016680
      00016690
      00016700
      00016710
      00016720
      00016730
      00016740
      00016750
      00016760
      00016770
      00016780
      00016790
      00016800
      00016810
      00016820
      00016830
      00016840
      00016850
      00016860
      00016870
      00016880
      00016890
      00016900
      00016910
      00016920
      00016930
      00016940
      00016950
      00016960
      00016970
      00016980
      00016990
      00017000
      00017010
      00017020
      00017030
      00017040
      00017050
      00017060
      00017070
      00017080
      00017090
      00017100
      00017110

```

H#H+1
 CIEFF(M,I)=CIEFF(M+1,I)
 NPROD(M,I)=20040
 210 IF(X,M,E,21) GO TO 220
 H#H+1
 CIEFF(M,I)=CIEFF(M+1,I)
 NPROD(M,I)=10000
 220 CONTINUE
 230 IF(TH00(NHCLT, 190, E0, 0)) GO TO 250
 DO 240 K=1,M
 240 NPROD(K,I)=NPROD(K,I)+1
 250 HMAX(I)=M
 IF(H,GT,7) PRINT 9039, H
 DISCT)=#A1
 GO TO 40
 260 ILITE = I+1
 IACT=0
 C
 C READ DATA FOR ACTINIDES
 C
 270 READ(R,9034,END=450)NUCL(I),DEAH,TU,FRT,FP,FP1,FT,FA,FSF,
 1GET,I,FG(I),DUMMM,AMPC(I),AMPC(I)
 DO 280 N=1,NLIRE
 READ(R,9037) SIGNG,RING,ENG1,SIGF,RIF,STGFF,SIGN2N,FN2N1,SIGN3N,IT00017350
 280 CONTINUE
 IF(1,I,E0,0) GO TO 300
 DO 290 N=1,N1
 290 READ(R,9036) SKIP
 300 IF(1T,EQ,0) GO TO 270
 310 H#0
 NUCLI=NUCL(I)
 IF(NUCLI,E0,0) GO TO 450
 DO 320 K=1,S
 IF(NUCLI,E0,NSURS(K)) NSURS(K)=I
 320 CONTINUE
 CALL HALF(I1,I1)
 CALL NOAH(NUCLI,NAME)
 SIGNG=THERM*SIGNG+RES*RING
 SIGF =THERM*SIGF +RES*RIF +FAST*SIGFF
 SIGN2N=SIGN2N*FAST
 SIGN3N=SIGN3N*FAST
 IF(MOD(IACT,50),E0,0) PRINT 9012, (TITLE (N),N=1,18)
 330 IF(MOD(IACT,50),E0,0) PRINT 9024
 PRINT 9026, NAME, DEAH,FRT,FP,FP1,FT,FA,FSF,SIGNG,00017550
 1 FNG1,STGF,SIGN2N,SIGN3N,WT(I),FG(I)
 340 IACT=IACT+1
 C
 C TEST RADIOACTIVITY
 C
 IF(A1,LT,ERR) GO TO 380
 ARETA=1.0
 C TEST POSITRON EMISSION
 IF(FP ,LT, ERR) GO TO 350
 ARETA=ARETA-FP
 H#H+1
 CIEFF(M,I)=FP*A1
 NPROD(M,I)=NUCL+10000
 C POSITRON EMISSION TO EXCITED STATE
 IF(FP1 ,LT, ERR) GO TO 350
 H#H+1
 CIEFF(M,I)=FP1*CIEFF(M+1,I)

```

NPROD(M,I)=NPROD(M+1,I)+1          00017730
CDEFF(M+1,I)=CDEFF(M+1,I)+CDEFF(M,I) 00017740
C ISOMERIC TRANSITION               00017750
350 IF(FT .LT. ERR) GO TO 360        00017760
M=M+1                               00017770
CDEFF(M,I)=FT*A1                   00017780
NPROD(M,I)=NUCLI                   00017790
A=BETA*BETA=FT                      00017800
C ALPHA EMISSION                   00017810
360 IF(FA .LT. ERR) GO TO 370        00017820
M=M+1                               00017830
CDEFF(M,I)=FA*A1                   00017840
NPROD(M,I)=NUCLI=20040              00017850
M=M+1                               00017860
CDEFF(M,I)=CDEFF(M+1,I)             00017870
NPROD(M,I)=20040                   00017880
A=BETA*BETA=FA                      00017890
C BETA DECAY                         00017900
370 IF(ABETA .LT. 1.E-4) GO TO 380   00017910
M=M+1                               00017920
CDEFF(M,I)=BETA*A1                  00017930
NPROD(M,I)=NUCLI+10000              00017940
TR(FR1 .LT. ERR) GO TO 380         00017950
M=M+1                               00017960
CDEFF(M,I)=CDEFF(M+1,I)*FR1        00017970
CDEFF(M+1,I)=CDEFF(M+1,I)+CDEFF(M,I) 00017980
NPROD(M,I)=NPROD(M+1,I)+1          00017990
C C NEUTRON CAPTURE CROSS SECTIONS
380 KAP(I)=M                        00018000
DO 390 K=1,6                         00018010
  CAPT(K)=0.0                         00018020
390 CAPT(2)=SIGNG*FNG1                00018030
  CAPT(1)=SIGNG*CAPT(2)                00018040
  CAPT(4)=SIGN2N*FN2N1                 00018050
  CAPT(3)=SIGN2N*CAPT(4)                00018060
400 FIRS(IACT)=SIGF                  00018100
TICAP(I)=0.0                          00018110
DO 410 K=1,4                         00018120
  CAPKI=CAPT(K)                      00018130
  IF(CAPKI .LT. ERR) GO TO 410       00018140
  M=M+1                               00018150
  TICAP(I)=TICAP(I)+CAPKI            00018160
  CDEFF(M,I)=CAPKI                   00018170
  NPROD(M,I)=NUCLI+NUCAL(K+2)        00018180
410 CONTINUE                           00018190
TICAP(I)=TICAP(I)+FISS(IACT)        00018200
C N=3N CROSS SECTION                 00018210
A17=SIGN3N                           00018220
IF(A17 .LT. ERR) GO TO 420          00018230
M=M+1                               00018240
CDEFF(M,I)= A17                      00018250
NPROD(M,I)= NUCLI=20                 00018260
TICAP(I)=TICAP(I)+A17                00018270
420 IF(NOD(NUCLI,10).EQ.0) GO TO 440  00018280
DO 430 K=1,M                         00018290
430 NPROD(K,I)=NPROD(K,I)+1          00018300
440 MMAX(I)=M                         00018310
IF(M.GT.7) PRINT 9039, M             00018320
  BUNF(IACT)*FSF*A1*I5.023E23      00018330

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ALPHANUMERIC)@FAXA1&H.(23E13*G(I)*3.65
DISC(I)=AI
I=I+1
GO TO 270
450 DO 460 K=1,5
460 TFLU(K)=0.0
C READ DATA FOR FISSION PRODUCTS
C
C 470 READ(A,9034,END=901)NUCL(I),DLAM,TU,FRI,FP,FPI,FT,FA,FSF,
10(I),FG(I),DUMMY,XNPCI(I),XNPCI(I)
9034 NBL,NLTHE
9035A READ(A,9035A) SIGNA,RING,FG1,Y,IT
10(I),E,I,O) GO TO 500
DO 490 READ(B,9036) SKIP
490 READ(B,9036) SKIP
500 IF(IIT .EQ. 0) GO TO 470
510 H=0
CALL HALF(A,I,I)
520 NUCLI=NUCL(I)
TFLU(NUCL,I,EQ,0) GO TO 690
CALL "DAH(NUCL,NAME)
TFLU(NUCL,50),EQ,0) PRINT 9012, (TITLE (N),#118)
SIGMATHERM=BIG+G+RES+RING
IF(LTHE*E0.3) GO TO 540
IF(NOT TL *50),EQ,0) PRINT 9010
PRINT 9021, NAME,
1 FG1,Y,Q(I),FG(I)
1 GO TO 550
540 IF(TDOL(1,50),EQ,0) PRINT 9020
PRINT 9022, NAME,
1 Y(2),Y(4),Y(5),Q(I),FG(I)

C TEST RADIOACTIVITY
C
C 550 IF(ALLLT,ERR) GO TO 600
APETIAS=0
C POSITION EMISSION
A3#FP
1 IF(LA3,L,ERR) GO TO 570
APETATABT=0.3
APETAS=FP1
APETAS=FP1
1 IF(LA3,L,ERR) GO TO 560
H=H+1
COEFF(N,I)=APETAS
NPROD(N,I)=NUCL*I*9999
560 IF(CAP1LT,ERR) GO TO 570
H=H+1
COEFF(N,I)=AP1*41
NPROD(N,I)=NUCL*10000
C ISO-EWIC TRANSITION
570 IF(LT ,LT ,ERR) GO TO 580
H=H+1
COEFF(N,I)=APETAS
NPROD(N,I)=NUCL*9999
APETATABT=FT
APETATABT=FT
NEGATRUE EMISSION
C 580 IF(CAP1LT,LT,ERR) GO TO 600
A2#FH1
00018340
00018350
00018360
00018370
00018380
00018390
00018400
00018410
00018420
00018430
00018440
00018450
00018460
00018470
00018480
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00018920
00018930
00018940

```


DO 710 K=1,XMAX
IF(NUCLI,NE,NPROD(M,J)) GO TO 710
NONO(I)=NONO(I)+1
NON=NON+1
IF(NON,GT,2500) PRINT 9041, NON,NUCL(I)
A(NON)=CDEFF(M,J)
JT=J
LOC(NON)=JT

710 CONTINUE

720 CONTINUE

KO(I)=NONO(I)

DO 740 J=1,ILITE

K=KAP(J)+1

KMAX=MMAX(J)

IF(KMAX,LT,K1) GO TO 740

DO 730 M=1,XMAX

IF(NUCLI,NE,NPROD(M,J)) GO TO 730

NONO(I)=NONO(I)+1

NON=NON+1

IF(NON,GT,2500) PRINT 9041, NON,NUCL(I)

A(NON)=CDEFF(M,J)

JT=J

LOC(NON)=JT

730 CONTINUE

740 CONTINUE

750 CONTINUE

C C NON-ZERO MATRIX ELEMENTS FOR THE ACTINIDES

C

650 760 IF(IACT,LT,1) GO TO 820

I=ILITE+1

I=ILITE+IACT

DO 810 I=ID,I1

NUCL(I)=NUCL(I)

DO 780 J=ID,I1

M=MAX(KAP(J))

IF(MAX,LT,1) GO TO 780

DO 770 M=1,MAX

IF(NUCLI,NE,NPROD(M,J)) GO TO 770

NONO(I)=NONO(I)+1

NON=NON+1

IF(NON,GT,2500) PRINT 9041, NON,NUCL(I)

A(NON)=CDEFF(M,J)

JT=J

LOC(NON)=JT

770 CONTINUE

780 CONTINUE

KO(I)=NONO(I)

DO 800 J=ID,I1

M=KAP(J)+1

M2=MMAX(J)

IF(M2,LT,M1) GO TO 800

DO 790 M=M1,M2

IF(NUCLI,NE,NPROD(M,J)) GO TO 790

NONO(I)=NONO(I)+1

NON=NON+1

IF(NON,GT,2500) PRINT 9041, NON,NUCL(I)

A(NON)=CDEFF(M,J)

JT=J

LOC(NON)=JT

790 CONTINUE

00019580
00019570
00019580
00019590
00019600
00019610
00019620
00019630
00019640
00019650
00019660
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00019680
00019690
00019700
00019710
00019720
00019730
00019740
00019750
00019760
00019770
00019780
00019790
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00019890
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00019940
00019950
00019960
00019970
00019980
00019990
00020000
00020010
00020020
00020030
00020040
00020050
00020060
00020070
00020080
00020090
00020100
00020110
00020120
00020130
00020140
00020150
00020160

```

800 CONTINUE
810 CONTINUE
C MATRIX ELEMENTS FOR FISSION PRODUCTS
C
820 IF(IFP.LT.1) GO TO 900
1=MLITE+IACT
IF(1.LT.1) GO TO 900
DO 830 I=MN,1,I+1
NUCL=NUCL(I)
I2=MAX(1,I-1,MN)
I3=MIN(1,I+1,I+10)
DO 840 J=I2,I3
KMAX=KAP(J)
IP(KMAX,LT,1) GO TO 840
DO 850 K=1,KMAX
IF(NUCL.NE.0)PRINT(4,J) GO TO 850
NONOT(NONOT(I)+1)
NONM(NM+1)
IF(NON.GT.2500) PRINT 9041,
AC(NON)*CDEF(4,J)
JTO J
LOC(4)=J
CONTINUE
830 CONTINUE
840 CONTINUE
K=NULO(I)
DO 860 J=I2,I3
K=KAP(J)+1
KMAX=MAX(X(J),
IP(KMAX,LT,X1) GO TO 860
DO 850 K=1,KMAX
IF(NUCL.NE.0)PRINT(4,J) GO TO 850
NONOT(NONOT(I)+1)
NONM(NM+1)
IF(NON.GT.2500) PRINT 9041,
AC(NON)*CDEF(4,J)
JTO J
LOC(4)=J
CONTINUE
850 CONTINUE
860 CONTINUE
IF(IACT.LT.1) GO TO 880
DO M70 K=1,S
IL=IIM
IF(YIELD(K,IL).LT.ERR) GO TO 870
NONM(NM+1)
IF(NON.GT.2500) PRINT 9041,
NONOT(NONOT(I)+1)
KMAX=KAP(K)
LOC(4)=K
KMAX=IL
AC(NON)*YIELD(K,IL)*FISS(4F)
CONTINUE
870 CONTINUE
880 CONTINUE
IF(IFP.LE.0) GO TO 900
IF(MLINE.NE.3) GO TO 890
PRINT 9027,
TYLD(2),TYLD(4),TYLD(5)
GO TO 900
900 PRINT 9030,
(TYLD(1),I=1,5)
C ALL MATRIX ELEMENTS ARE NOW COMPUTED

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4611 PERGAMON PRESS (1961)1,1,1 D T GOLDFAR AND JAMES R RISER 00021390
 51CHART OF THE NUCLEUSES NINTH EDITION GENERAL ELECTRIC CO (JULY 00021400
 61968)1,1,1 E O ARNOLD FIPROGRAM SPECTRUM APPENDIX A OF DRNL-3576 00021410
 71APRIL 1964)1,1,1 00021420
 9010 FORMAT(1, CROSS SECTIONS AND FLUX SPECTRA,1,1 R E PRINCE 11NEUT00021430
 1IRON REACTION RATES IN THE MSRE SPECTRUM DRNL-4119, PR 79483 (JUL 00021440
 2Y 1967)1,1,1 R E PRINCE 11NEUTRON ENERGY SPECTRA IN MSRE AND MSRR 00021450
 31 DRNL-4191, PR 50-58 (DEC 1967)1,1,1 H D GOLDFARB ET AL 11NEUTRON 00021460
 4CROSS SECTIONS DRNL-325, SECOND ED, SUPP NO 2 (MAY 1964 * AIG 390021470
 5661 ALSO EARLIER EDITIONS,1,1,1 H T KERR, UNPUBLISHED ERC COMPILATION 00021480
 6DN (FEB 1968)1,1,1 H K DRAKE 11A COMPILATION OF RESONANCE INTEGRAL 00021490
 7811 NUCLEONICS, VOL 24, NO 8, PR 108-111 (AUG 1968)1,1,1 DRNL STAF 00021500
 8RF 11INVESTIGATION OF N-2N CROSS SECTION 11BNF-98, PR 44-98 (JUNE 00021510
 91965)1,1,1 00021520
 9011 FORMAT(18A4,T3) 00021530
 9012 FORMAT(1H1,20X,18A9) 00021540
 9013 FORMAT(1 H ALTER AND C E WEBER 11PRODUCTION OF H AND HE IN METALS 00021550
 1DURING REACTOR IRRADIATION 11 J NUCL MATLS, VOL 16, PR 68-73 (1965)00021560
 21,1,1 L L BENNETT 11RECOMMENDED FISSION PRODUCT CHAINS FOR USE IN 00021570
 3REACTOR EVALUATION STUDIES DRNL-1658 (SEPT 1965)1,1,1 00021580
 9014 FORMAT(1, FISSION PRODUCT YIELDS,1,1 M E MEIK AND H F RIDER, 1100021590
 1SUMMARY OF FISSION PRODUCT YIELDS FOR U-235, U-238, Pu-239, AND Pu00021600
 2-241 AT THERMAL FISSION SPECTRUM AND 1,1,1 14 MEV NEUTRON ENERGY 00021610
 3E811 APED-39B-A(CREV.), OCT. 1968)1,1,1 B KATCOFF 11 FISSION PRODUCT00021620
 4YIELDS FROM NEUTRON INDUCED FISSION 11NUCLEONICS, VOL 18, NO 11, 00021630
 5NOV 1960)1,1,1 N D DUDEY 11 REVIEW OF LOXAHASS ATOM PRODUCTION IN 00021640
 6A87 REACTORS 11ANL-7434 (APRIL 1968) 1,1,1 00021650
 9015 FORMAT(1H0,20X,1LIGHT ELEMENTS, MATERIALS OF CONSTRUCTION, AND ACT00021660
 1IVATION PRODUCTS 1,1,10 NUCL DEAM FB1 FP FP1 FT 00021670
 2A SIGNG FNGL FNGL RIF RIF FNGL FNGL SIGMEV FN2H100021680
 3 FNGL FPFP R FG1) 00021690
 9016 FORMAT(1H0,20X,1LIGHT ELEMENTS, MATERIALS OF CONSTRUCTION, AND ACT00021700
 1IVATION PRODUCTS 1,1,10 NUCL DEAM FB1 FP FP1 FT 00021710
 2A SIGNG FNGL SIGNG FN2M1 SIGNA SIGNP R FG AH100021720
 3NANCE)1,1,1 00021730
 9017 FORMAT(1H ,A2,13,41,1PE9,2,0PSE6,3,1PE9,2,0P3F6,3,1PE9,2,0P2F6,3, 00021740
 11PE9,2,0P4F6,3,0P5,2) 00021750
 9018 FORMAT(1H0,10X,1THEME 1P10,5,5X,1HESE 1F10,5,5X,1FAST 1F10,5, 00021760
 11,1,1,1NEUTRON SOURCE 15(10,5X),5X,1NLTRB 1I3) 00021770
 9019 FORMAT(1H0,38X,1FISSION PRODUCTS 1,1,10 NUCL DEAM FB1 FP 00021780
 1 FP1 FT SIGNG 1, 1 FNGL Y23 Y25 Y02 00021790
 228 Y49 R FG1) 00021800
 9020 FORMAT(1H0,38X,1FISSION PRODUCTS 1,1,10 NUCL DEAM FB1 FP 00021810
 1 FP1 FT SIGNG FNGL Y25 Y26 Y49 R FG1) 00021820
 9021 FORMAT(1H ,A2,13,41,1PE9,2,0P4F6,3, 1PE9,2,0P6,3,1PSE9,2, 00021830
 10P2F6,3) 00021840
 9022 FORMAT(1H ,A2,13,41,1PE9,2,0P4F6,3,1PE9,2,0P6,3,1PSE9,2,0P2F6,3) 00021850
 9023 FORMAT(1H0,32X,1ACTINIDES AND THEIR DAUGHTERS 1,1,1 00021860
 1 NUCL DEAM FB1 FP FP1 FT FA FSF E+6 SIGNG 00021870
 2ING FNGL SIGNR RIF SIGNF SIGN2N SIGN3N R FG100021880
 9024 FORMAT(1H0,32X,1ACTINIDES AND THEIR DAUGHTERS 1,1,1 00021890
 1 NUCL DEAM FB1 FP FP1 FT FA FSF E+6 SIGNG 00021900
 2NG21 SIGNF SIGN2N SIGN3N R FG1) 00021910
 9025 FORMAT(1H ,A2,13,41,1PE9,2,0PSE6,3,0P6,1,1P2F9,2,0P6,3,1PSE9,2, 00021920
 1 0P6,3,FS,2) 00021930
 9026 FORMAT(1H ,A2,13,41,1PE9,2,0PSE6,3,0P6,1,1PE9,2,0P6,3,1P3E9,2, 00021940
 1 0P7,3,FS,2) 00021950
 9027 FORMAT(10SUM OF YIELDS OF ALL FISSION PRODUCTS 1,15X,1P3E9,2) 00021960
 9028 FORMAT(15,2X,1PE10,3,3X,E10,3,5(2X,E10,3,3X,151/(30X,5(2X,E10,3, 00021970
 1 3X,15))) 00021980
 9029 PRK-AT(1NON-ZERO MATRIX ELEMENTS AND THEIR LOCATIONS)1,1,1 00021990


```

DATA STA/1,1,1,1,1/
END
SUBROUTINE HALF(L)
C   SUBROUTINE HALF Converts HALF-LIFE TO DECAY CONSTANT (1/SEC)
DIMENSION C(9)
DATA C/b,9315F+01,1.1552E+02,1.9254E+04,8.0226E+06,2.1965E+08,0.+
1.2*1965E+11,2.165E+14,2.1965E+17/
1 IF(L.GT.0) GO TO 10
IF(L.EQ.0) GO TO 20
A=9.99
RETURN
10 A=C(1)/A
RETURN
20 A=0
RETURN
END
SUBROUTINE NUANTNUCL1(NAME)
C   SUBROUTINE NUANT Converts SIX DIGIT IDENTIFIER TO ALPHAMERIC SYMBOL
INTEGER#2 NAME(3)
INTEGER#2 FILE(9),STA(2)
COMMON/LAFL/ ELE,STA
IS=ORD(NUCL1,10)+1
NZ =NUCL1/10000
NAME(1)=NAME(1)*NZ *1000
NAME(1)=FILE(NZ)
NAME(2)=NAME(2)*W
NAME(3)=STA(19)
RETURN
END

```

CHAPTER 4. DATA NEEDED FOR RADIOACTIVE SOURCE TERM
CALCULATIONS FOR BOILING WATER REACTORS (BWRs)

This chapter lists the information needed to generate source terms for BWRs. The information is provided by the applicant and should be consistent with the contents of the Safety Analysis Report (SAR) and the Environmental Report (ER) of the proposed boiling water reactor. This information is the basic data required to calculate the releases of radioactive material in liquid and gaseous effluents (the source terms). All data is on a per-reactor basis.

4.1 GENERAL

1. The maximum core thermal power (Mwt) evaluated for safety considerations in the SAR.
(Note: All of the following responses should be adjusted to this power level.)
2. The quantity of tritium released in liquid and gaseous effluents (Ci/yr per reactor).

4.2 NUCLEAR STEAM SUPPLY SYSTEM

1. Total steam flow rate (in lb/hr).
2. Mass of reactor coolant (in lb) in the reactor vessel at full power.

4.3 REACTOR COOLANT CLEANUP SYSTEM

1. Average flow rate (in lb/hr).
2. Demineralizer type (deep bed or powdered resin) and size (in ft³).
3. Regeneration or replacement frequency.
4. Regenerant volume (in gal/event) and activity (if applicable).

4.4 COMPENSATE DEMINERALIZERS

1. Average flow rate (in lb/hr).
2. Demineralizer type (deep bed or powdered resin).
3. Number and size (in ft³) of demineralizers.
4. Regeneration or replacement frequency.
5. Indicate whether ultrasonic resin cleaning is used and waste liquid volume associated with its use.
6. Regenerant volume (in gal/event) and activity.

4.5 LIQUID WASTE PROCESSING SYSTEMS

1. For each liquid waste processing system, provide in tabular form the following information:
 - a. Sources, flow rates (in gal/day), and expected activities (fraction of primary coolant activity, i.e., PCA) for all inputs to each system.
 - b. Holdup times associated with collection, processing, and discharge of all liquid streams.
 - c. Capacities of all tanks (in gal) and processing equipment (in gal/day) considered in calculating holdup times.
 - d. Decontamination factors for each processing step.

- e. Fraction of each processing stream expected to be discharged over the life of the plant.
 - f. For waste demineralizer regeneration, the time between regenerations, regenerant volumes and activities, treatment of regenerants, and fractions of regenerant discharged. Include parameters used in making these determinations.
 - g. Liquid source term by radionuclide (in Ci/yr) for normal operation, including anticipated operational occurrences.
2. Provide piping and instrumentation diagrams and process flow diagrams for the liquid radwaste systems, along with all other systems influencing the source term calculations.

4.6 MAIN CONDENSER AND TURBINE GLAND SEAL AIR REMOVAL SYSTEMS

- 1. The holdup time (in hr) for offgases from the main condenser air ejector prior to processing by the offgas treatment system.
- 2. A description and the expected performance of the gaseous waste treatment systems for the offgases from the condenser air ejector and mechanical vacuum pump. The expected air inleakage per condenser shell, the number of condenser shells, and the iodine source term from the condenser.
- 3. The mass of charcoal (in tons) in the charcoal delay system used to treat the offgases from the main condenser air ejector, the operating and dew point temperatures of the delay system, and the dynamic adsorption coefficients for Xe and Kr.
- 4. A description of the cryogenic distillation system, the fraction of gases partitioned during distillation, the holdup in the system, storage following distillation, and the expected system leakage rate.
- 5. The steam flow (in lb/hr) to the turbine gland seal and the source of the steam (primary or auxiliary).
- 6. The design holdup time (in hr) for gas vented from the gland seal condenser, the iodine partition factor for the condenser, and the fraction of radioiodine released through the system vent. A description of the treatment system used to reduce radio-iodine and particulate releases from the gland seal system.
- 7. Piping and instrumentation diagrams and process flow diagrams for the gaseous waste treatment system, along with all other systems influencing the source term calculations.

4.7 VENTILATION AND EXHAUST SYSTEMS

For each plant building housing the main condenser evacuation system, the turbine gland seal system exhaust, or any system that contains radioactive materials, provide the following:

- 1. Provisions incorporated to reduce radioactivity releases through the ventilation or exhaust systems.
- 2. Decontamination factors assumed and the bases (include charcoal adsorbers, HEPA filters, and mechanical devices).
- 3. Release rates for radioiodines, noble gases, and radioactive particulates (in Ci/yr); radioactive particulate size distribution; and the bases.
- 4. Release point description including height above grade, height above and location relative to adjacent structures, expected average temperature difference between gaseous effluents and ambient air, flow rate, exit velocity, and size and shape of flow orifice.
- 5. For the containment building, indicate the expected purge and venting frequencies and duration and the continuous purge rate (if used).

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