

NUCLEAR REQULATORY COMMISSION WASHINGTON, D. C. 20555

MEMORANDUM FOR:

Edson Case, NRR

John Davis, 1&E

FROM:

John Ahearne

SUBJECT:

RESTART OF DAVIS-BESSE UNIT 1

Attached for your information and review are copies of two analyses of the September 24, 1977, incident at Davis-Besse, one by Babcock and Wilcox, the other apparently by the licensee. I note that the B&W papel is labelled 'Advance Copy," so there may have been a later version. would appreciate any comments you may have on these analyses, particularly how they may relate to the Three Mile Island accident.

I understand that I&E has requested that Metropolitan Edison not restart Davis-Besse Unit 1 without first notifying I&E, and that this restart is tentatively scheduled for sometime in the April 9-10 time frame. Since the reports from the operators of B&W plants called for in the IE Bulleti 79-05, Nuclear Incident at Three Mile Island, sent on April 1 are due at about that same time, I strongly recommend that Metropolitan Edison be requested not to restart Unit 1 until NRC has received and reviewed these responses for whatever implications they may have on further operation of Unit 1.

Attachments

cc: Chairman Hendrie Commissioner Gilinaky Commissioner Kennedy Commissioner Bradford SECY

EDO

Serial No. 475 December 22, 1978 Page Three

Of these two transients the loss of feedwater results in the greater volumetric coolant contraction, because the forced coolant flow (RC Pumps operating) causes a faster rate of heat rejection to the steam generator.

1. Loss of Offsite Power

Preliminary calculations for a reactor trip following a loss of offsite power show that the pressurizer loses indication but does not empty. The assumptions used to derive this result included full runout auxiliary feedwater flow (~2400 gpm) resulting in a fill time to 120" of about 4 minutes. No net mass change to the primary coolant (no makeup, no letdown) was considered, even thou the makeup controls would respond to decreasing pressurizer level by increasing the net input to above 200 gpm. At the termination of the transient the pressurizer level is slightly above the outlinto the surge line. Reactor coolant pressure reaches about 1600 and high pressure injection may be automatically initiated.

Although the net makeup was not considered, it would in fact caus the pressurizer to refill to the normal level. At the same time compression of the steam would cause a partial repressurization of the system ensuring that the coolant remains subcooled. This trapresents no safety concerns.

2. Loss of Feedwater

This transient has a greater reactor coolent contraction than the loss of offsite power case, resulting in emptying of the pressuri Consequently it will be described in greater detail.

A brief summary of the events is:

· Reactor trip

Time = 0

 Makeup control valve opens wide admitting full makeup to reactor coolant system

Time = 0+

. AFW initiated

Time 240 se

 Pressurizer empties; RC system pressure slightly greater than 1800 psi

Time ≈ 2 min

· HPI initiated by SFAS; makeup isolated

Time 2 2 mis

 Steam generator level = 10 ft; voids exist in reactor coolant

Time 24 min

 HPI inflow replaces volume occupied by voids; pressurizer leval begins to be restored

Time \$27-8 mit

95004015

3+3 = charine from mucheste

1-8.2-2-2

Frether what pumps times of O. THI

الم السلم المال المال المال

Bra meries

The major concerns that evolve from this transient are the disposition of the steam voids and the approach to DNB. Both of the concerns are analierated by the reactor coolant pumps.

License No. NPT-3 Serial No. 475 December 22, 1978 Page Four

Steam voids will not collect in reactor coolant piping and no flow blockage will occur because of dispersal and mixing by the forced flow. DNF acceptance criterion limit will be met because the power output of the core is at the decay heat level and all reactor pumps are operating, maintaining core heat removal. We conclude that no safety problem exists.

TABLE 1: STEAM AND FEEDWATER LINE RUPTURE CONTROL SYSTEM (SFROS) ACTUATION PARAMETERS

Act	tuation Parameter		Accident
Sta	etion Variables	Setpoint	
1.	Low'Steam Line Pressure	< 591.6 psig ¹ 2 ²	Steam Line Break Feedwater Line B:
2.	Low SG Level	≤ 17 inches¹	Loss of F/W
3.	SG Pressure Minus Nein Feedwater Line Pressu	> 197.6 psi ¹	FWLB, LONFW
4.	Loss of All RC Pumps ³		Loss of Off-Site

NOTES:

- When actuated, STRCS closes both main steam isolation valves, closes to main FW control and stop valves, initiates AFW and controls AFW to main a 120 inch level in the SCs.
- 2. Alignment of AFW to a pressurised SS is provided for steam and feedwate line breaks.
- 3. AFW initiation but steam and feedwater line isolation does not occur.

Operator to Control Feedwater Level at 35"

Introduction:

The following bounding analysis conservatively predicts the events occurring within the primary reactor coolant system and reactor following a loss of main feedwater from 100% power for the Davis-Besse Unit 1. Auxiliary feedwater control has been assumed at 10 feet within both steam generators.

Results:

Because of the conservative, bounding, nature of this calculation, the overcooling of the primary system due to auxiliary feedwater injection causes a contraction of coolant volume sufficient to create steam within the primary system. The steam is shown to be uniformly distributed within the RCS and the void fraction is 4%. The reactor coolant pumps maintain full capability. The DNB ratio is shown to exceed 2.0 and no return to criticality potential exists. Thus, during the course of the incident, no core problems develop. Further, following the time of maximum contraction, the system recovers to full pressure, pressurizer function is regained and the reactor coolant returns to a subcooled water configuration without operator action.

Analysis:

The following assumptions have been made to assure the bounding mature of the results:

Reactor Power:

100% until boiling stops in the steem generators; 0% after that time. This assumption is conservative as core heat would compensate for the cooling caused by the auxiliary feedwater.

Initial Coolant Inventories Water:

RCS = 11290 ft3

Pressurizer = 864 ft³

These assumptions are nominal operating values.

Initial Temperatures:

The whole system is taken to be at T everage = 582°F.

This assumption is a reasonable average.

Initial System Mass: ~ 500,000 1bm

The mass is figured from the temperature and volumes above.

Makeup System:

No credit is taken for additional makeup flow which will occur as the pressurizer loses level. (In all likelihood, the makeup system will contribute approximately 200 ft extra liquid volume).

local Power (kw/ft): 18.4 kw/ft

This value is taken as the maximum allowed by Technical Specifications.

Secondary Side Volume At 10 Foot Level

711 ft3 per generator, actual volume.

Auxiliary Feedwater Flow:

166.5 ft3/min. per generator actual value.

Auxiliary Feedwater Enthalpy:

8 Btu/1bm lower bound for maximum cooling.

With the initiating event, loss of main feedwater, the reactor coolant system pressure will start to rise. Reactor trip will occur on high RCS pressure. Following trip, the RCS pressure will fall because core power has been reduced and boiling of residual main feedwater or auxiliary feedwater is occurring in the steam generators. These events are almost identical to those which occur in a main feed line break and are analyzed in detail in Section 15.2.8 of the FSAR.

In short order, the system will return to its initial configuration but, because the auxiliary feedwater heat absorption rate exceeds the decay heat generation rate, the RCS continues to depressurize. During this phase, residual main feedwater and injected auxiliary feedwater will be boiled and vented through the steam generator safety relief valves. The primary system average temperature will fall to the saturation temperature of water at the safety valve set pressure. At this time, primary and secondary conditions are expected to be approximately as follows:

	Primery .	Secondary
Pressure	1800 psia	, 980 psia
Temperature	542 F	542 F
Mass	503344 1bm	0 1bm
Liquid Volume in Press.	400 ft ³	N.A.
Time into Transient	½ 2 mim.	<u>~</u> 2 min.

It is conservative to assume complete boiling of the secondary side water and complete equilibrium between primary and secondary sides, as these assumptions load to the maximum follow on injection of auxiliary feedwater and therefore, maximum contraction. RCS pressure is held up by the steam bubble in the pressurizer.

The time has been estimated by calculating the necessary energy loss by the primary system from its initial conditions, the mass of auxiliary feedwater required to remove this energy and then dividing by the auxiliary feedwater flow rate.

time $\simeq \frac{(586 - 542) \ 503344}{(1194-8) \ 3$3 \ 62} \simeq 54$ sec.

Six seconds was used to estimate the initial pressurization portion of the transient.

In performing the remainder of the evaluation 10 feet of cooled (40 F) auxiliary feedwater is placed in each steam generator and the thermal equilibrium condition calculated. Because after a 10 foot level is obtained this auxiliary feedwater flow stops, this condition represents the maximum contraction possible. The state variables resulting are:

	Primary	Secondary
Pressure	560 psia	560 psia
Temperature	478 F	478 F
Enthalpy of Water	462 B:u/lbm	462 Bru/15=
Specific Volume	.020 ft ³ /1bm	.020 fr ³ /1bm

From the specific volume, the primary liquid volume can be calculated: $\text{Vol} = \text{NV}_f = 10052 \text{ ft}^3$

As 10052 is smaller than the RCS minus pressurizer volume, the remaining volume must be filled with steam.

 $V_{st} = 10426 - 10552 = 374 \text{ ft}^3 \approx 400 \text{ ft}^3$

400 ft³ corresponds to a system void fraction of 3.8% ~ 4%, and as will be shown later, is of no consequence as far as core heating or system performance is concerned. This steam volume is larger than actually expected for two reasons: 1) some temperature difference would always exist between the primary and secondary systems, and 2) the effect of core decay heat has been ignored. Both of these would increase the primary side liquid temperature, thus increasing its volume and reducing the steam volume.

Following this state of maximum contraction, no further heat is removed from the RCS via the secondary side until the RCS rises in temperature due to decay heating; this will expand the liquid volume, compress the steam and repressurize the RCS. As no mass can be lost from the secondary

system prior to achieving 980 psia the first reheating stage will end at a primary system pressure, temperature, and liquid volume of 980 psia, 3 542 F, 10832 ft. Subtracting 10426 from 10832 shows that about 400 ft. of fluid has been forced back into the pressurizer. Pressurizer function would then be restored (if not directly, then, by either the makeup or MPI system), the RCS subcooled and the transient ended.

Several questions exist about the transient:

- How is the 400 ft dispersed within the primary system and can that volume collect in one location? From the auxiliary feedwater flow rate, over 4 minutes are required to fill the generators. As the pressurizer has 400 ft in it at 980 psis and the RCS has 400 ft in it at maximum contraction, approximately 2 minutes are used to eject steam from the pressurizer to the RCS. Because this steam will be superheated when it enters the RCS it will first desuperheat and then condense at a rate governed by its expending pressure compared to the contraction of the liquid coolant. In the time of 2 minutes the reactor coolant will have made about 8 complete circles of the primary system and the steam can be considered well mixed. As the flow velocity in the RCS will remain normal, about 25 ft/sec, steam water separation will tend not to occur. Some limited steam accumulation may occur in the upper head of the reactor vessel as in that specific location of the RCS, velocity is low.
- II. How well will the pumps work? Experiments performed on steam carry over capability show that for void fractions up to 10% no loss of pump capability is observed. This is documented in Figure 5-47 of BAW-10104, "DiN's ECCS Evaluation Report With Specific Application to 177 FA Class Plants With Lower Loop Arrangement." Actually pump capability increases for the first 5% of void introduced into the system.
- III. Will any return to power be encountered because of the low RCS temperature? A return to power can occur for a non-borated core at 490F. This temperature includes the assumption of the most reactive rod stuck out of the core; if that rod were taken as inserted the critical temperature would fall to at or below 400F. Although no credit was taken for HPI in calculating the RC steam volume below 1600 psia, the HPI will be injecting borated water and, therefore, preventing any return to power condition. If the primary system were to stabilize at 1600 psia and thus prevent the HPI from providing boron the RCS temperature would be at least 511F and, therefore, no return to power would be expected.
- IV. Will DNB be encountered in the core? The maximum contraction condition is again:

P - 560 psia

T = 478F

a = 4%.

In order to expedite submittel of your report, we are sending Sections Λ , this time, as agreed in our telecon of October 24. We expect to forward Section & by-November 7, and we will try to improve on this date.

Section A describes the sequence of events as reconstructed from computer alarm printout, reactimeter plots, and control room recorders (Attachment [A.1]). We have attached pertinent recorder charts of T, RC pressure, pressurizer level (Attachments A2; A3 at A4) and reactimeter plots of RC falet temperature, RCS flow in each loop, RC pressure; Inlet temperature, RCS flow in each loop, RC pressure, pressurizor level, and water level and outlet pressure of each eteam generator thereanments A5 through A13).

Section B will include evaluations of stresses in the pressure boundary, the depressuri tion transient, boiling the SG dry, jet impingement of the SG, and effect upon fatigue life.

Section C explains the evaluation which was performed to verify that there was no significant damage to RC pump bearings, seals, or impellers (attachment Cl). The transient as it affected the pumps is summarized in Attachment C2. Attachment C3 defines the instrumentation and operational checks applied to the pumps. The results of the operational checks are tabulated in Attachment C4.

Section D evaluates the effect upon the core to determine (1) whether steam was produced in the core (2) the maximum internal fuel rod pressure, and (3) whether maximum lift force exceeded the limit (Attachment D.1). Reactimeter plots are attached for reference Attachments D.2 through D.6.

Very truly yours,

A. H. Lazar Senior Project Manager

JAL/hj

Attachments

j/ A. Lauer Project Manager

Minnewer A.

Sequence of Events

The event started at time 21:34:20 on September 24, 1977. The plant was in Mode 1 with Power (MwT) = 263. The turbine had been shutdown eatlier in the evening to repair a leak in the main steam line at an instrument connection between the turbine stop valves and the high pressure turbine. At this time a half trip of the Steam and Feedwater Rupture Control System (SFRCS) was initiated by an unknown cause. This trip shut the startup feedwater valve to #2 steam generator and stopped all feedwater to this generator (because of the low power level the main feedwater block valve was already shut, isolating the main feedwater control valve). The low level alarm was reached in #2 steam generator at 21:34:44. Before the operator could identify and correct the problem, the low level in #2 steam generator produced a full trip of the SFRCS. This trip shut the main steam isolation valves and feedwater isolation valves in both steam generators (time 21:35:18). SFRCS also started both auxiliary feedwater pumps. The number one pump performed as intended, however, number two auxiliary feedwater pump only came up to 2600 RPM, insufficient to feed its steam generator (#2).

The loss of feedwater, first to one and then both steam generators, caused an increase in primary water temperature, which resulted in an increase in pressurizer level and thus reactor coolant system pressure. At 2255 PSIG the pressurizer electromatic relief valve received an open signal. During the next 40 reconds, it received nine different open and close signals. After one of those signals the valve stuck open. This provided a continuous 2½" vent path from the pressurizer to the quench tank. When pressurizer level got to 290", the operator manually tripped the reactor (time 21:36:07). Energy escaping from the electromatic relief valve and three main steam relief valves caused a rapid cooldown and depressurization of the reactor coolant system. Reactor coolant system pressure dropped to 1600 PSIG (time 21:37:17) initiating the Safety Features Actuation System (SFAS). This started high pressure injection and closed numerous containment isolation valves, including the quench tank cooling lines.

With the electromatic relief valve still open and cooling water isolated to the quanch tank, the quench tank rupture disc ruptured (time 21:40) relieving water/steam to the containment building. This discharge damaged a nearby ventilation duct, was deflected off this duct and directed onto #2 steam generator. The steam tore off approximately a 10' high x 20' circumferential sec' on of insulation from #2 steam generator. The paint from the then exposed area of the steam generator was blasted away. Other indirectors of systems interaction due to the steam in the containment include two fire alarms (one near RCP 2-2 and one near the pressurizer) and a single channel RPS trip on high reactor building pressure (4 PSIG).

When the (main steam relief valves reseated the decrease in reactor coolant system temperature stopped and the high pressure injection pumps started to raise prossurizor level. At time 21:40:34 the operator stopped the high pressure injection pumps. (The operators had been heavily involved before this time in regaining scal injection flow to the reactor coolant pumps. This flow had been stopped by the SFAS actuation. By 21:39:40 the appropriate SFAS signals had been overriden and normal flows restored to the seals of the pumps). Reactor coolant system pressure continued to decrease until saturation pressure was reached and steam began to form in the RCS (approximate time 21:42). This caused an insurge of water into the pressurizer and pressurizer level want off scale high at 320 inches. During this level increase the operator, seeing average reactor coolant system temperature and pressurizer level increasing, stopped one reactor coolant pump in each loop (time 21:43:11).

Due to ducreasing pressure in 0.2 steam generator, the SFRCS system gave a low pressure block permit signal at time 21:48:33. This alerted the operator to the low level and feed condition of 0.2 steam generator. He blocked the low pressure trip (time 21:49:38), took manual control of the speed of 0.2 suxiliary feedwater pump and fed 0.2 generator (time 21:50). The operator saw the rapid addition of cold feedwater dropping the reactor coolant system temperature and stopped the feedwater addition to this generator.

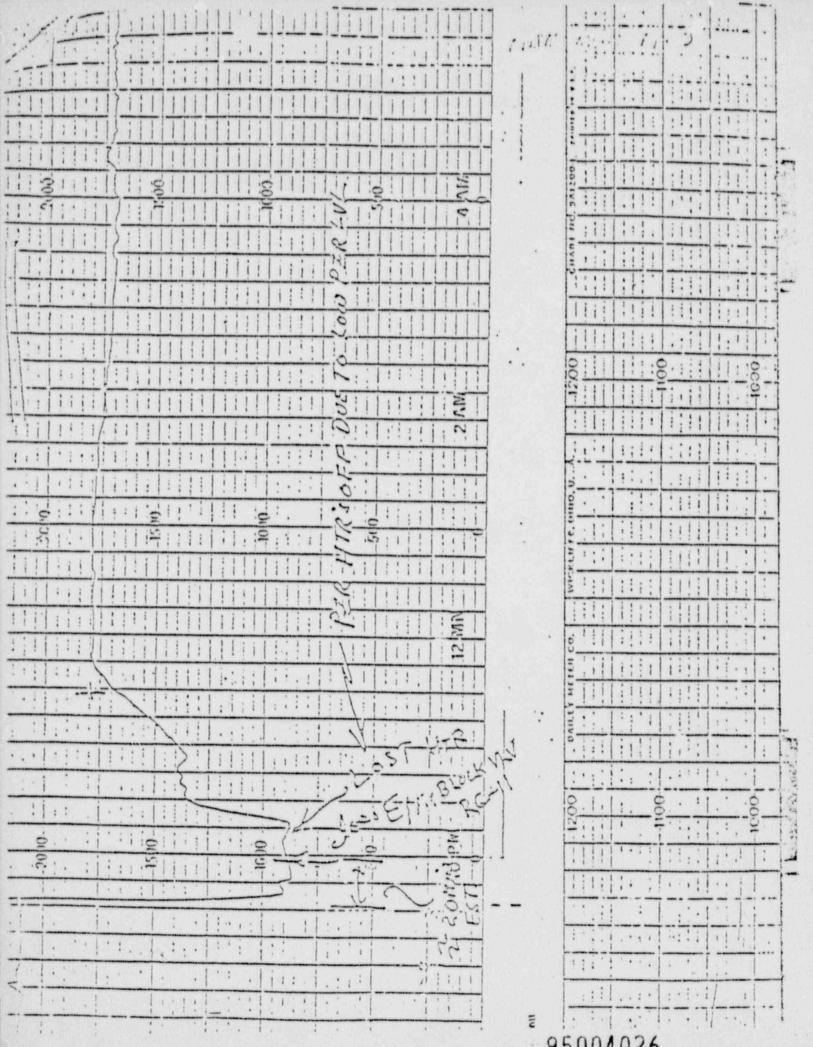
At approximately 21:55 the operator shut the block valve for the electromatic relief valve on the pressurizer and stopped the venting of the reactor coolant system to the quench tank. At 22:05 pressurizer level came back on scale. At 22:15 the operator started a second makeup pump to try and stop the pressurizer level decrease. This additional cold water started the reactor coolant system on a slow decreasing temperature transient. At 22:17 pressurizer level reached the low level interlock and cut off the pressurizer heaters. At 22:23 the operator started a high pressure injection pump to try and stop the decreasing pressurizer level.

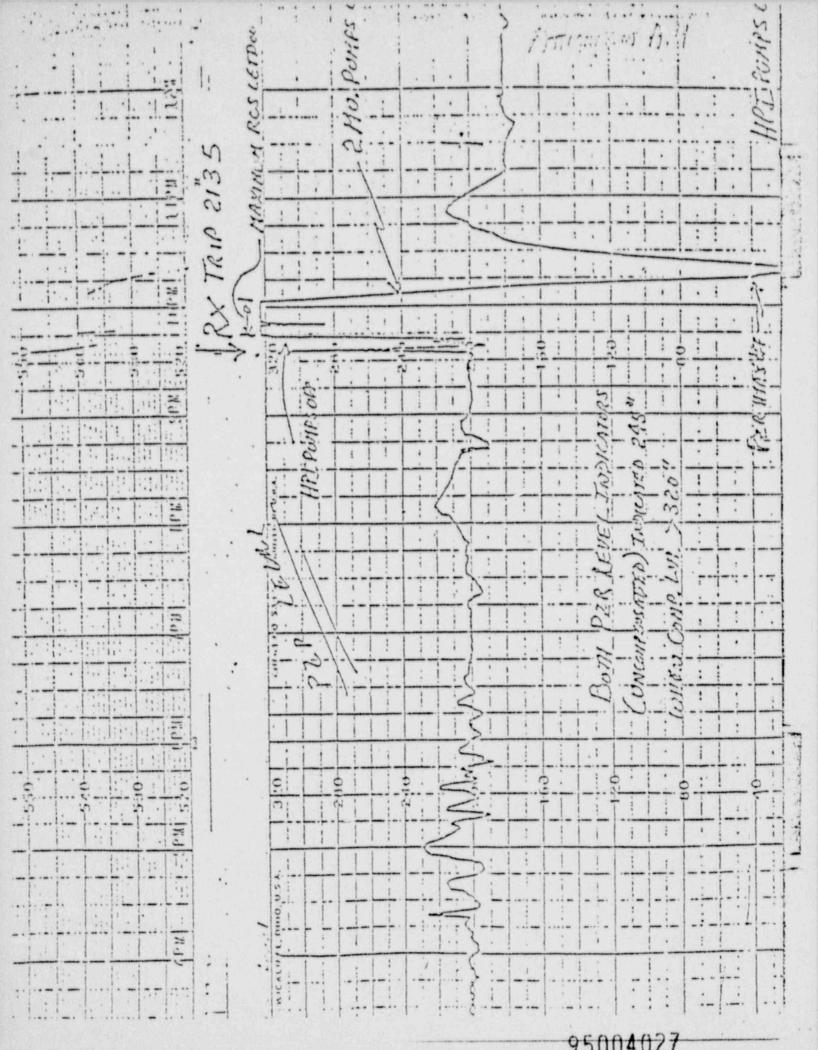
The Alevel and pressure in #2 steam generator again decreased to the point where the STRCS gave a low pressure block permit signal. The operator again blocked the trip and, through manual speed control of its auxiliary feedwater pump, restored level and pressure in #2 steam generator (time 22.25).

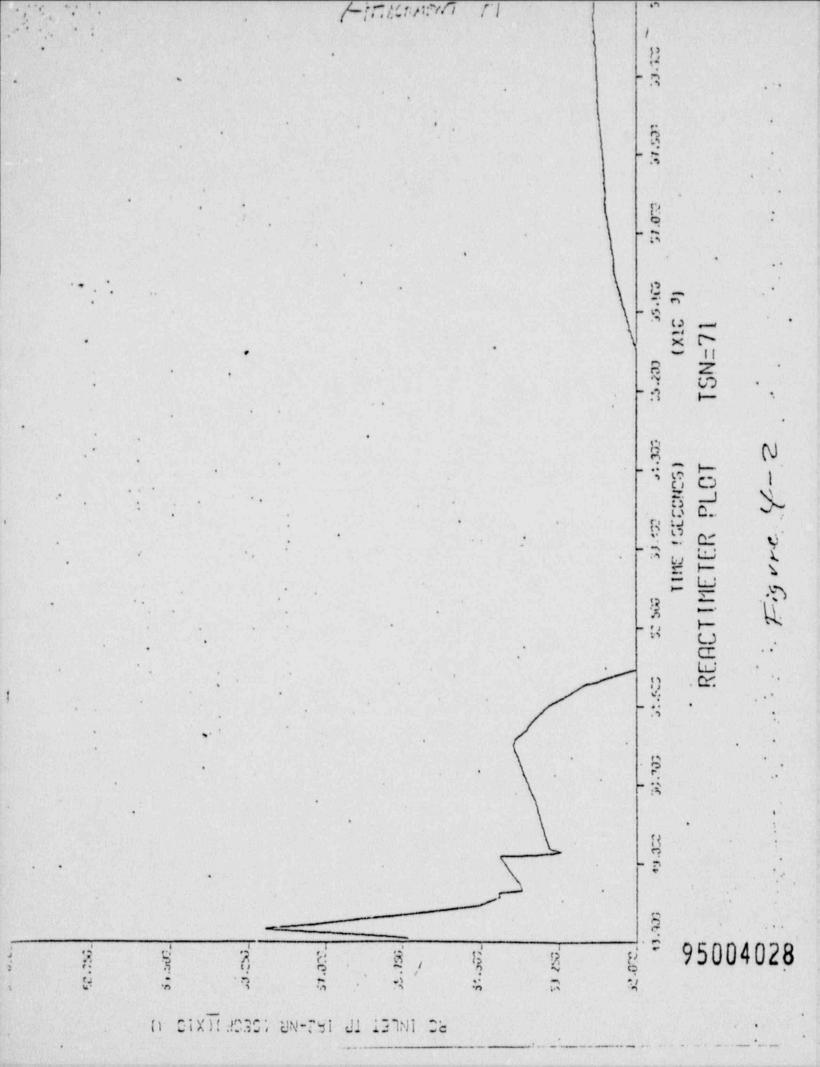
With pressurizer level well on its way to recovering, the operator stopped the high pressure injection pump (time 22:27:44). At time 22:31 he restored RC makeup flow to normal. This stopped the slow decreasing RC temperature transient started at time 22:15. All plant parameters were now fully under control and the plant was brought to a steady state condition and a normal plant cooldown started.

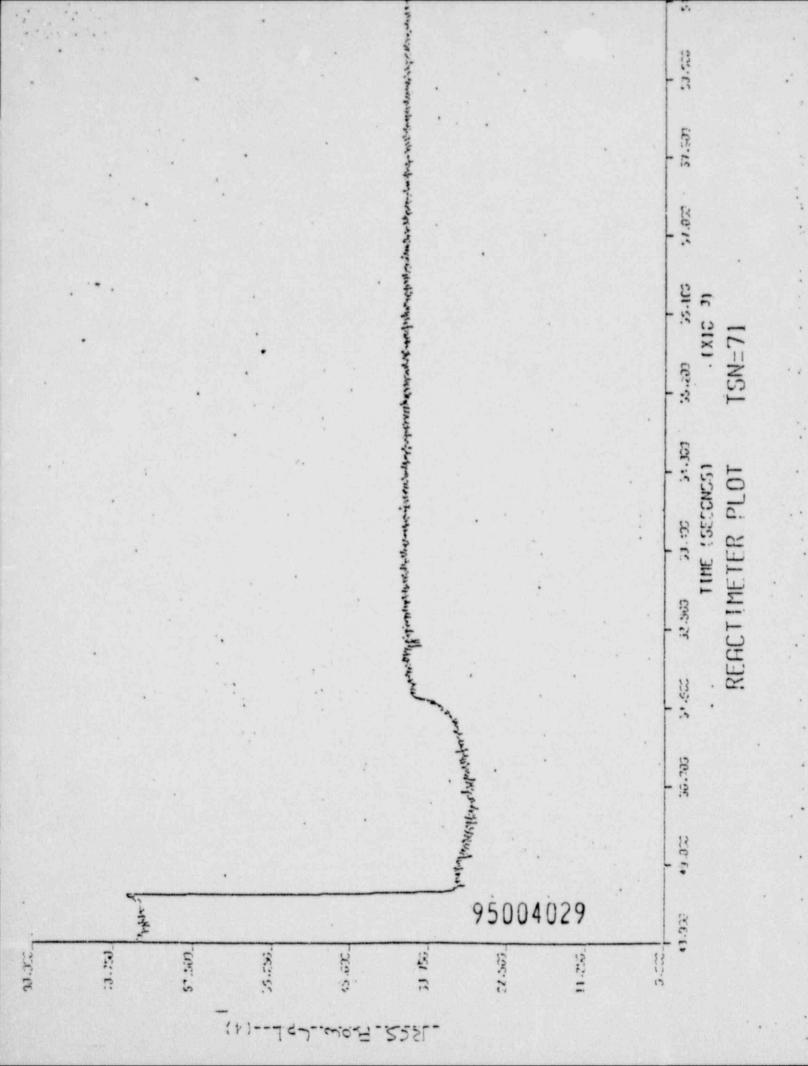
1,174500 10 .TH

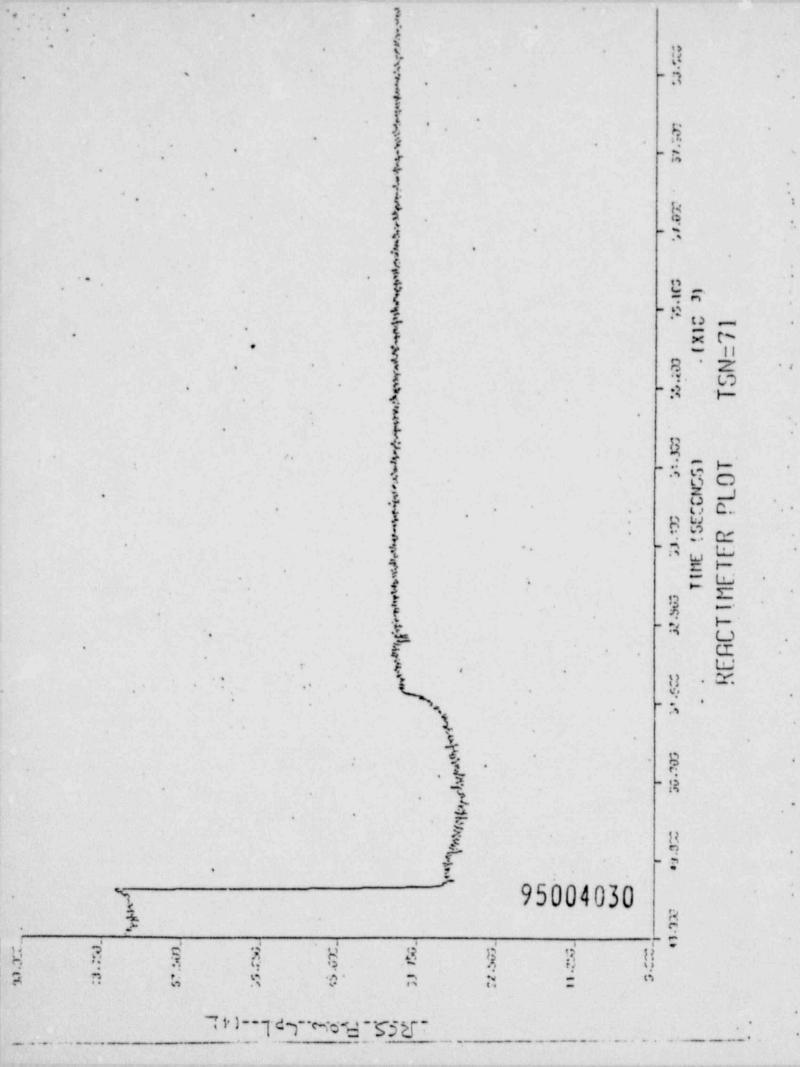
32/11/11.		;	
			1 22.75
	2 (36	168 -	
W. C. 12.10	Tarp 3	\$05 -	
1			
1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1			
		950	04025

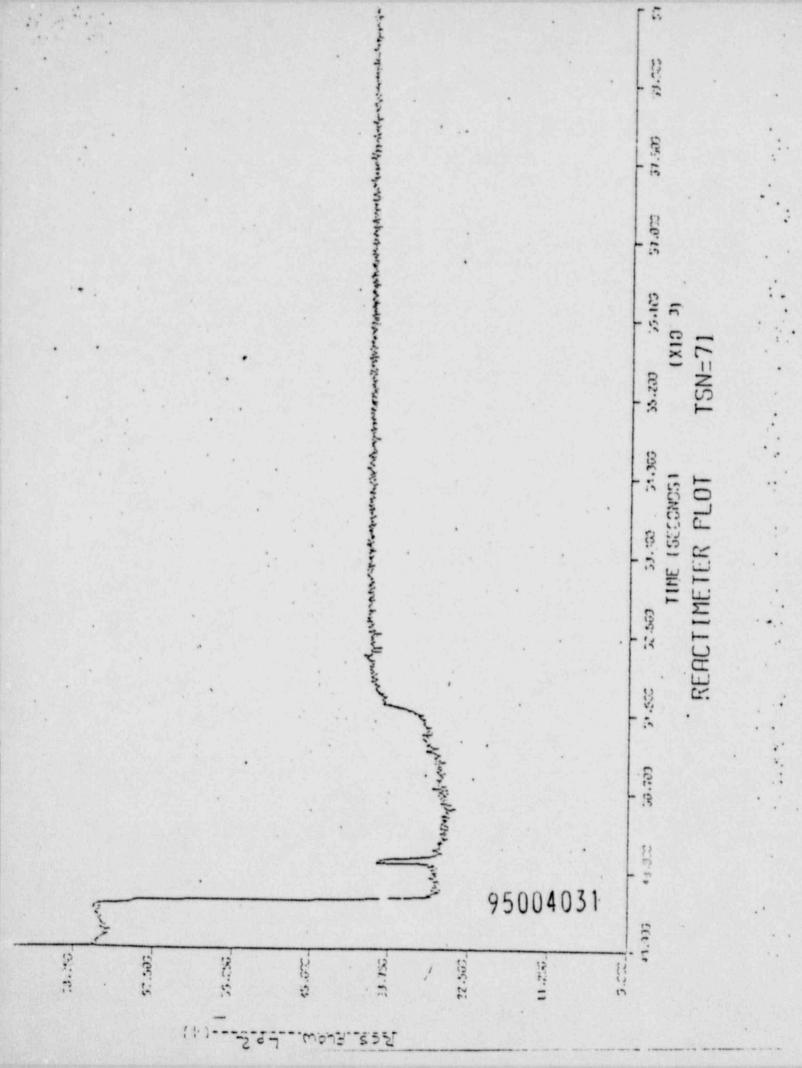


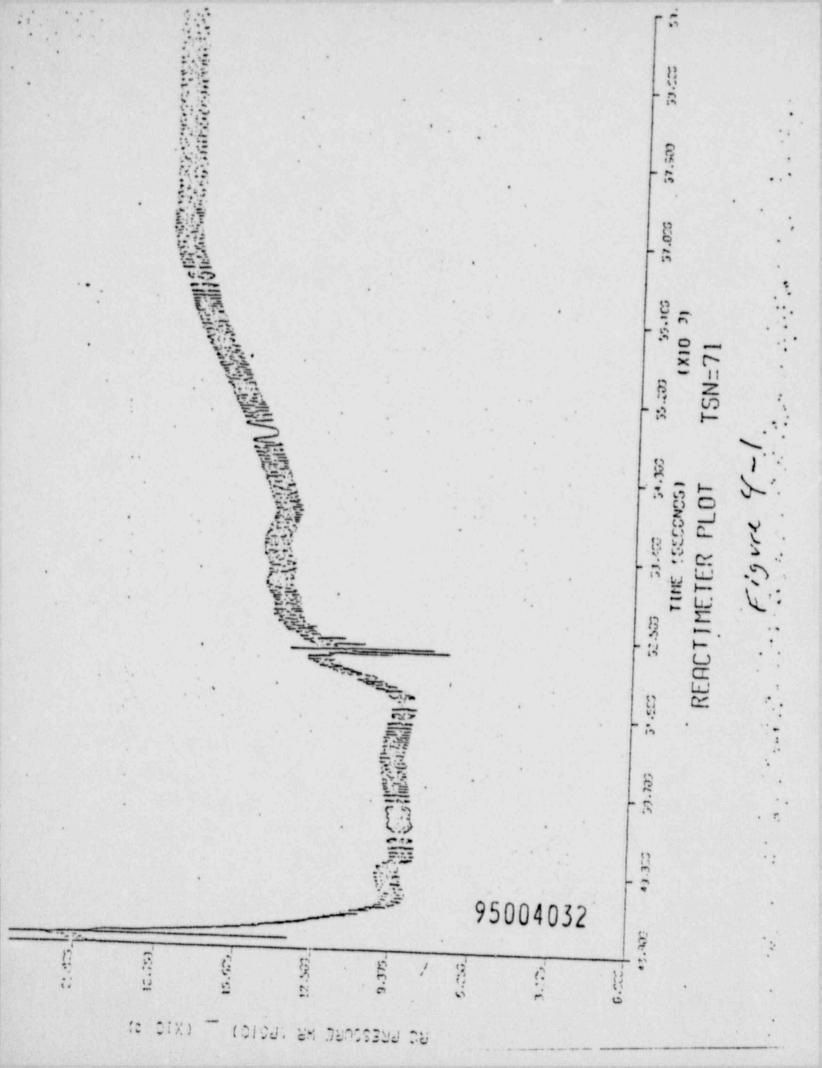


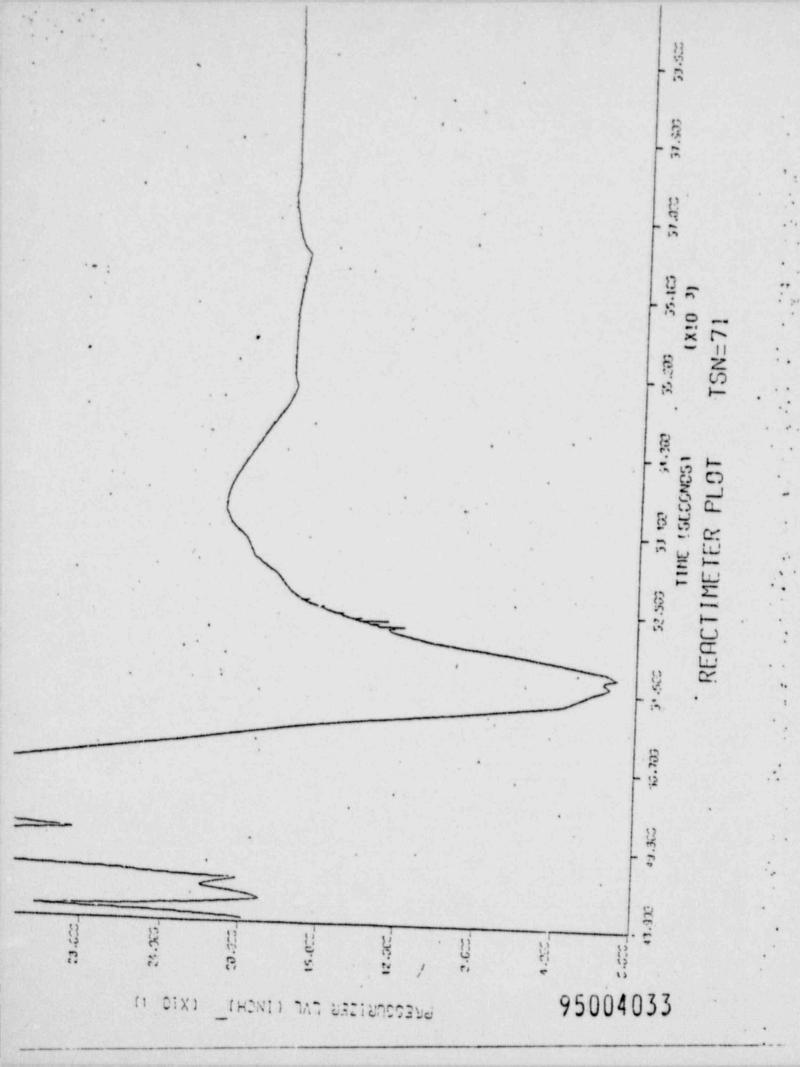


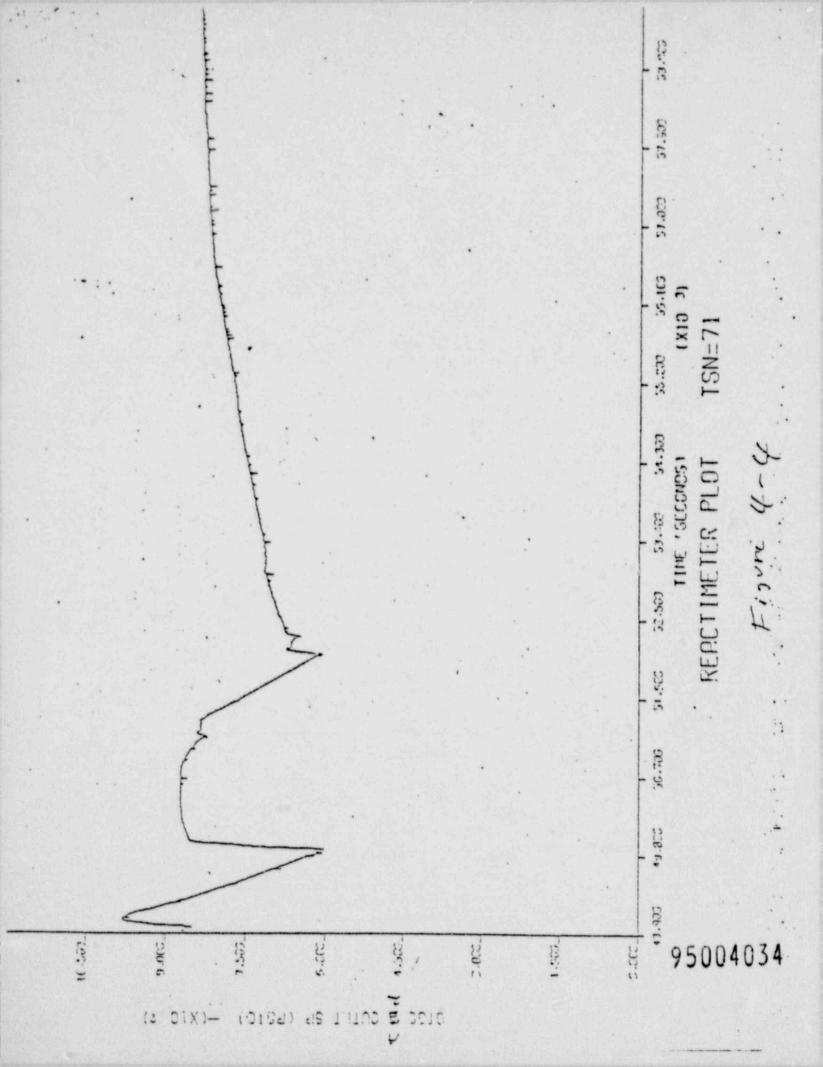


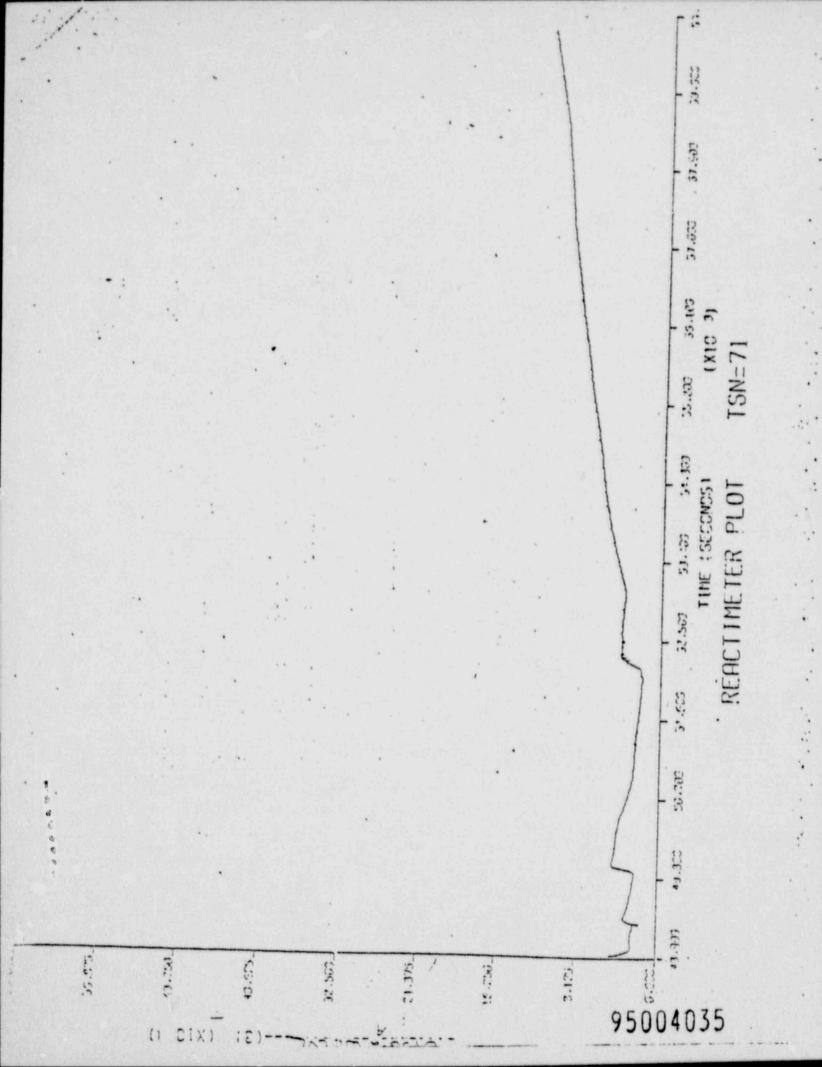


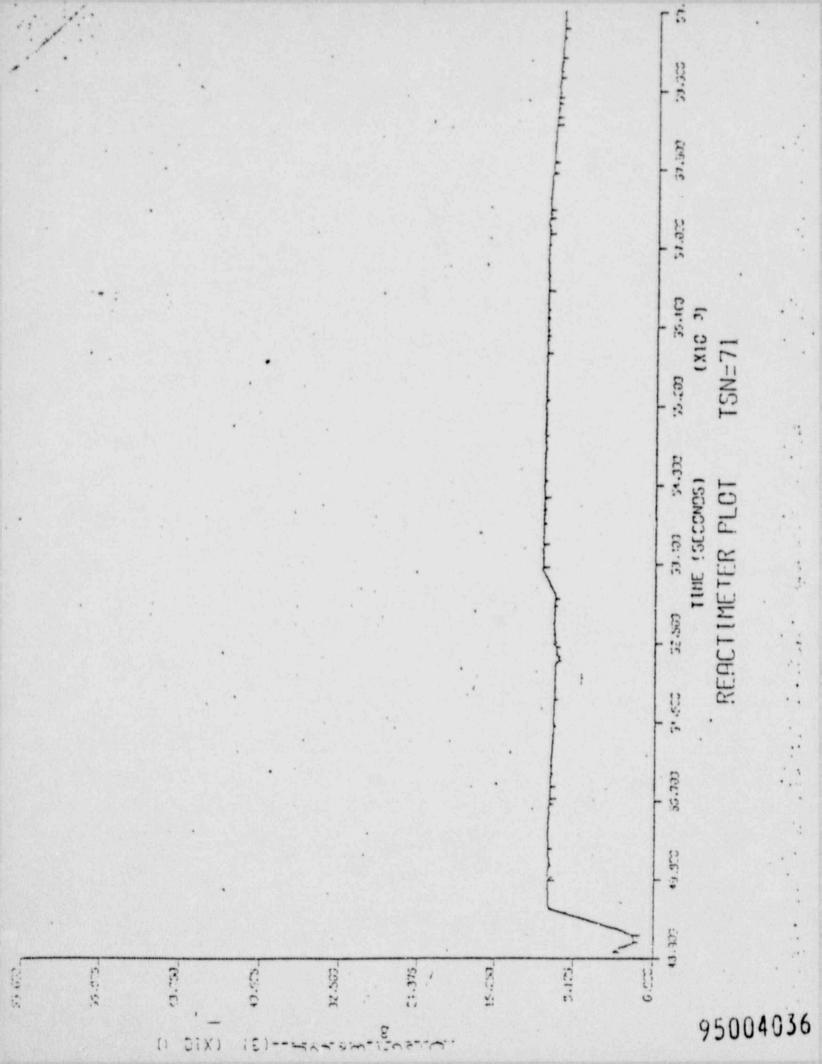


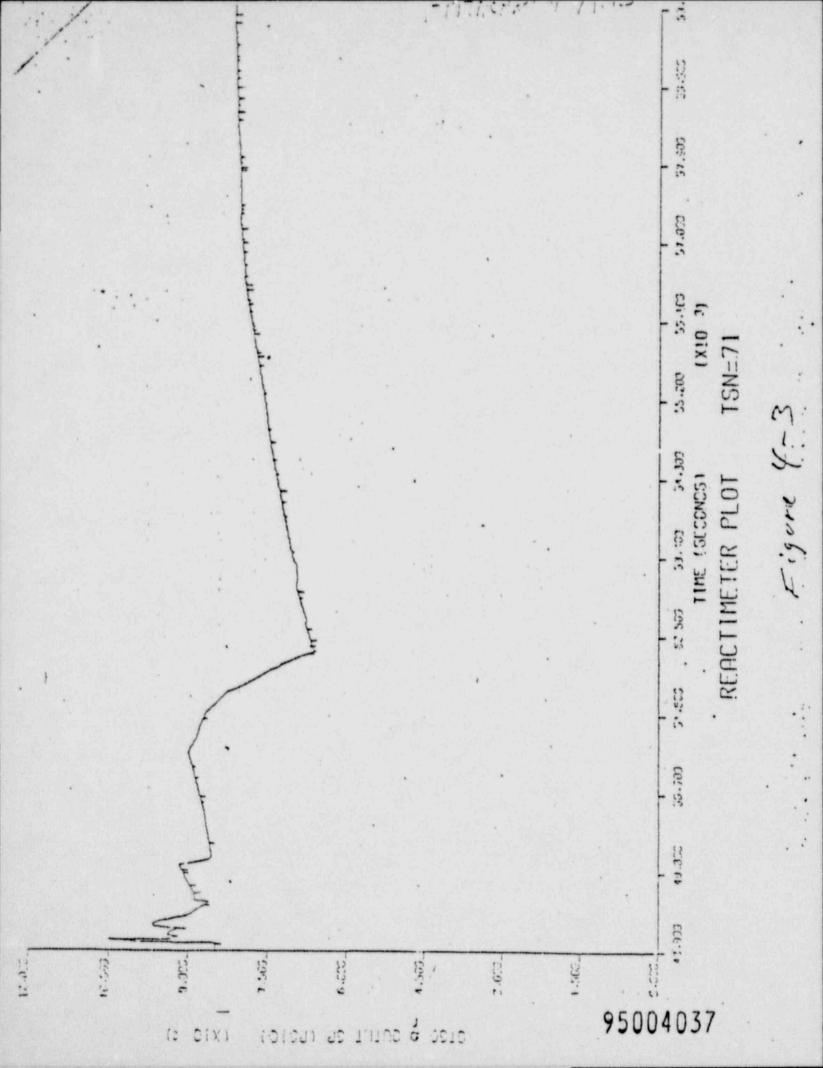












RC PUMPS

As a result of the September 24 abnormal system transient, the reactor coolant pumps experienced the conditions outlined in Attachment C.2. In order to checks were performed as outlined in Attachment C.3. The results of the operational operational checks are described in Attachment C.4.

BAW has reviewed the results of the operational checks and concluded that no detectable damage has occurred to the pump components. BAW finds the pumps to be serviceable for sustained full operational conditions with no immediate.

It should be noted that a step increase in vertical vibration of 2-2 pump was observed during the initial low pressure checkout runs. This indication was later assessed to be spurious instrument noise as a result of a loose connector on instrument line. After the connector was tightened, vertical vibrations remained less than one quarter milé peak-to-peak amplitude.

RC PUMPS

SEPTEMBER 24 TRANSIENT . 0 . DB-1

All four RC pumps were subjected to the following:

0:00 1:10 1:12 1:13 7:28 3:05 6:00	Reactor trip SFAS trip Seal return valves shut for 1:16 Seal injection valves shut for 1:52 all four pumps operated for 1:15 with no seal injection and no seal return flow during an RCS Seal return valves open Seal injection valves open Steam formation
36:07	Total seal injection flow low alarmat for ~30 to 45 minutes

Pump 1-1:

7:04 7:45 36:07	Pump tripped Shaft stopped About one minute of low seal injection flow (near 2 gpm) flow imbalance starved seal injection	
36:30 1:12:55 :17:07	flow imbalance starved seal injection flow (near 2 gpm) Seal return valve shut Standpipe lavel high Standpipe level normal	

Pump 2-2:

7:04 36:07 36:22	- Pump Lost	vibration tripped seal injection for about one minute return valve shut for
	5681	return valve shut for about 40 seconds

PUPPOSE:

Assess whether maintenance is required of RC pumps as a result of abnormal transient of 9/21/77. Operational checks will be required to demonstrate that no significant damage has occurred to the pump bearings, shaft and seals. First series of tests will be performed in Node 5 due to operational restrictions by NRC. Later on operational checks will be performed in Mode 3. Each pump will be operated individually for a duration not to exceed ten (10) minutes, providing all defined parameters remain within limits established in this procedure.

Operational sequence will be as follows:

- 1. Lift pumps will be started and pump shafts rotated by hand. Torque values are not to exceed 200 ft-lbs. A stethoscope will be provided to detect any unusual mechanical noises in seal housing area. (This has been satisfactorily completed on 10/3/77).
- 2. Mode 5 testing 225 psig.
 - 2.1 Instrumentation Required . see attached (LA).
 - 2.2 Computer Data Printout NSS special summary trend for running RCP every 15 seconds.
 - 2.3 Following limits shall not be exceeded:
 - A. Shaft wibration 15 mills peak to yeak.
 - B. Total standpipe leakage (upper seal leakage) plus seal return should not exceed 0.6 gpm. If, during the test this limit 's exceeded, the possibility exists of an open seal. In no case will total seal leakage be allowed to exceed 1.5 gpm. If this limit is exceeded, maintenance will be required before further pump operation.
 - C. All other normal plant limits and procautions prevail.
 - 2.4 Sequence of Operation:
 - A. Secure standpipe flush.
 - B. Establish seal injection in accordance with plant operating procedure.
 - C. Measure and record standpipe leakage and return flow, confirm that total leakage limits are not excuaded.
 - D. Assure communication between control room and personnel stationed at DOP standpipe leakage drain line. 95004040
 - E. Countdown from 10 to 0

 Start atrip chart recorders at high speed;
 Start Resetor Coopert Pump 2-2 in accordance with plant op. procedure.

- y. Man pump for two (2) minutes walcos any above simits are exceeded.
- c. Data taken will be ansessed by Baw and B-J representatives.
- H. Following assensment of data, pump may be run for an additional five (5) minutes to allow for venting procedure requirements.
- I. Follow above sequence on 2-1, 1-2 and 1-1.
- J. Assessment of this data will determine whether any maintenance is required before higher pressure operation is allowed.

SIMILAR

3. Above test will be repeated with system pressure at greater than 1300 psig before final determination on condition of the pumps is completed.

CCE:nlf 10/5/77

- Upper and lower cavity pressures all four pumps.
- 2. Both horizontal B/N Vibration Probes all four pumps.
- WR System Pressure or suction pressure.
- Vertical probe on 2-2 pump.
- 5. Standpipe leakage will be collected and measured during the test.

NOTE: All of above should be recorded on an 8 channel brush recorder located

RFS:mlf 10/5/77

ATTICHERY C.

All four Reactor Coolant Pumps were run on 10/5/77, per the attached procedure, with the following results:

ROP 2-2 10/5/77 Pun (2 min.):

System pressure 225 psig 2nd Seal cavity pressure 165 psig 3rd Seal cavity pressure 123.9 psig Norizontal vibration 5 - 7.5 mills Vertical vibration .25 mills 3rd Seal leakage plus <. Lop=

After the two minute run, the pump was run for ten minutes for system venting. About 30 seconds before the pump was shutdown, there was a step increase in vention vibration to 2.5 mills. The pump was run again on 10/6/77 for 10 minutes to checkout this phenomenon. The vertical vibration was again .25 mills until about 5 seconds before shutdown where it increased to 2.5 mills. To allow a longer run time, 2-1 and 2-2 pumps were run together for 10 minutes, then 2-2 was run alone for 10 minutes. The vertical vibration stayed at .25 mills for the entire run. This will continue to be monitored during pump runs for plant heat up.

PCP 2-1

System pressure 225 psig 2nd Seal cavity pressure 132 psig 3rd Seal cavity pressure 70 psig Horizontal vibration 5 - 7.5 mills 3rd Seal leakage plus

RCP 1-2

System pressure 225 psig 2nd Seal cavity pressure 40.29 psig 3rd Seal cavity pressure 81.3 psig Horizontal vibration 5 - 7.5 mills

3rd Seal leakage plus <.4 spn

RCP 1-1

System pressure 225 psig 2nd Seal cavity pressure 77.98 psig 3rd Seal cavity pressure 89.27 psig Horizontal vibration 5 - 7.5 mills

on 10/6/77 by installing pressure gauges at the pressure transmitters. The

1-1:

184.2nd cavity

1-2:

184-2nd cavity 112-3rd cavity

The readings indicate the seals are staging properly.

Based on the above performance, Baw sees no concern which would justify mainten-

Purther Testing to be Done:

- During heatup, contact B&W (R. F. Smith o. C. C. England) whenever TECo
 plans to start a RCP, so additional data can be taken at B&W's discretion.
- 2. At system pressure > 1300 psig, 3 pumps running, data will be taken on all four pumps.

10/7/77

STATUS OF CHECKOUT OF REACTOR COOLAGE PURPS: 10/13/77

All four RC Pumps have been run at system pressure greater than 1300 psi.
RC Pumps 2-1 and 2-2 have continued to run from the initial cold pump starts.
Below is a typical line of data from each pump.

RCP 2-1

System Pressure - 1650 psig 2nd Seal Cavity Pressure - 1074 psig 3rd Seal Cavity Pressure - 500 psig Eorizontal Vibration - 3 mils

RCP 2-2

System Pressure - 1650 psig 2nd Seal Cavity Pressure - 1075 psig 3rd Seal Cavity Pressure - 588 psig Korizontal Vibration - 3.5 mils

RCP 1-1

System pressure - 1650 psis 2nd Seal Cavity Pressure - 1056 psis 3rd Seal Cavity Pressure - 540 psis Horizontal Vibration - 4 mils

PCP 1-2 .

System Pressure - 1650 psig 2nd Seal Cavity Pressure - 920 psig 3rd Seal Cavity Pressure - 520 psig Eorizontal Vibration - 3 mils

Based on the above data, I feel that all four pumps are in good operating condition and require nothing more at this time than periodic monimoring.

EFE: n2.f 20/23/77 At Smith-

DB 1 CORE

ANALYSIS OF SEPTEMBER 24 DEPRESSURIZATION EVENT

A more detailed analysis was done to assess core thermal conditions during the Septembe 24 depressurization event at Davis-Besse 1. Core conditions were analyzed to (1) rod pressure during the transient, and (3) determine if maximum lift force exceeded the limit.

CORE COOLANT CONDITIONS

Attachment D.2 shows transient thermal conditions as monitored by the reactimeter. The system pressure is measured at the pressure tap, which is approximately 65 feet above the top of the core. The RC pressure at the top of the core is approximately 50 psi higher than the measured pressure because of unrecoverable and elevation pressure losses. As shown in Attachment D.3, the predicted core coolant temperature is slightly higher than the minimum saturation temperature (based upon measured pressure), however, there is some uncertainty in both the measurement and the prediction, therefore, it is possible that some vapor bubble formation (steam bubbles in water) could have occurred within the core. An examination of the reactimeter data (attachment D.4) indicates that the RCS pressure level was near the saturation pressure for less than one hour and that during this time period the pressure oscillated with a variation of ± 50 psi. Therefore, the maximum time period during which the core could have been subjected to bubbly flow was less than one hour. Approximately fifteen-minutes after reactor trip the coolant temperature dropped below the minimum -estimated saturation_temperature, therefore, the bubbly flow, if it-existed at-all. -Cocurred-for no-more than ten minutes. If bubbles were formed during this period, the formation would be in the liquid as well as on the surface, as opposed to formation from a hot surface. With the temperatures, time duration, and type of formation, no significant effect on the components would be predicted.

FUEL ROD PRESSURE

Prior to the depressurization event the reactor had been operating at 15% power for approximately one week. Immediately prior to reactor trip the power level was 9% of production had occurred and none was released. The maximum initial backfill pressure of this fuel was 465 psia at 70°F. During the 60 minute time period in which the indicate average coolant temperature was less than 540°F and no significant heat generation in the cladding based upon a maximum pressure differential across the cladding of 200 to safety factor added to ensure that actual conditions would be bounded by the prediction. The recent analysis, again using TAFY, has resulted in a predicted maximum internal across the cladding broader to properties and the rod pressure of 1000 psia. This analysis considered as-built fuel properties and the rod pressure of 1000 psia. This analysis considered as-built fuel properties and the rod pressure conditions at a coolant average temperature of 540°F. On the 4.4

pasis of this analysis it is concluded that the fuel rod cladding was not subjected to any significant level of tensile stress during the subject depressurization event.

Since the cladding was not subjected to a large, long term tensile stress, no significant long term effects on the cladding resulted. The tensile stresses which could have occurred would have little effect on the cladding due to the small stress level and the short duration of the tensile stress.

CORE LIFT

Assuming a coolant temperature of 537 F and 150 X 10⁶ lb/min system flow (per Attachments D.5 and D.6) the net lift force will be less than 375 lb. The maximum allowable lift force is 472.lb., therefore fuel assembly lift-off is not predicted:

We conclude that