

INTERIM REPORT

Accession No. \_\_\_\_\_

Contract Program or Project Title: Light Water Reactor Thermal Hydraulic Development Program

Subject of this Document: Informal Report, "Pressure and Void Distributions in a Converging-Diverging Nozzle with Nonequilibrium Water Vapor Generation"

Type of Document: Informal Report

Author(s): G. A. Zimmer, B.J.C. Wu, W. J. Leonhardt, N. Abuaf, and O. C. Jones, Jr.

Date of Document: April 1979

Responsible NRC Individual and NRC Office or Division: Dr. Y. Y. Hsu  
Division of Reactor Safety Research  
Systems Engineering Branch  
U.S. Nuclear Regulatory Commission  
Washington, D.C. 20555

This document was prepared primarily for preliminary or internal use. It has not received full review and approval. Since there may be substantive changes, this document should not be considered final.

NRC Research and Technical Assistance Report

Brookhaven National Laboratory  
Upton, NY 11973  
Associated Universities, Inc.  
for the  
U.S. Department of Energy

Prepared for  
U.S. Nuclear Regulatory Commission  
Washington, D. C. 20555  
Under Interagency Agreement EY-76-C-02-0016  
NRC FIN No. A-3045

INTERIM REPORT

575 019  
221  
7907110, 483

PRESSURE AND VOID DISTRIBUTIONS IN A CONVERGING-DIVERGING  
NOZZLE WITH NONEQUILIBRIUM WATER VAPOR GENERATION

G. A. ZIMMER, B.J.C. WU, W. J. LEONHARDT  
N. ABUAF AND O. C. JONES, JR.

REACTOR SAFETY EXPERIMENTAL MODELING GROUP

DATE PUBLISHED - APRIL 1979

DEPARTMENT OF NUCLEAR ENERGY BROOKHAVEN NATIONAL LABORATORY  
UPTON, NEW YORK 11973

NRC Research and Technical  
Assistance Report

Prepared for the U.S. Nuclear Regulatory Commission  
Office of Nuclear Regulatory Research  
Contract No. EY-76-C-02-0016



#### NOTICE

This report was prepared as an account of work sponsored by the United States Government. Neither the United States nor the United States Nuclear Regulatory Commission, nor any of their employees, nor any of their contractors, subcontractors, or their employees, makes any warranty, express or implied, or assumes any legal liability or responsibility for the accuracy, completeness or usefulness of any information, apparatus, product or process disclosed, or represents that its use would not infringe privately owned rights.

575 021

PRESSURE AND VOID DISTRIBUTIONS IN A CONVERGING-DIVERGING  
NOZZLE WITH NONEQUILIBRIUM WATER VAPOR GENERATION

By

C. A. Zimmer, B.J.C. Wu, W. J. Leonhardt  
N. Abuaf and O. C. Jones, Jr.

O. C. Jones, Jr.: Principal Investigator

Thermal Hydraulic Development Division  
Department of Nuclear Energy  
Brookhaven National Laboratory  
Upton, New York 11973

APRIL 1979

Prepared for the U.S. Nuclear Regulatory Commission  
Office of Nuclear Reactor Regulation  
Contract No. EY-76-C-02-0016  
FIN NO. A-3045

NOTICE: This document contains preliminary information and was prepared primarily for interim use. Since it may be subject to revision or correction and does not represent a final report, it should not be cited as reference without the expressed consent of the author(s).

## ABSTRACT

A steady water loop with well controlled flow and thermodynamic conditions was designed, built, and made operational for the measurement of the net vapor generation rates under nonequilibrium conditions. The test section consists of a converging-diverging nozzle with 49 pressure taps and observation window at the exit. Pressure distributions and photographic observations were recorded under various flashing conditions. The effect of the various parameters such as inlet pressure, inlet temperature, mass flux, and back pressure on the pressure distributions and flashing regimes was investigated and is reported here. For flashing under high back pressures, a sharp increase in pressure (condensation shock) was observed in the diverging section. For lower back pressures, although the pressure distributions in the converging section were identical to the single phase calibration data, a constant pressure region was observed all along the diverging section of the nozzle. With  $\gamma$ -densitometry, the chordal averaged void fraction profiles were also measured along the centerline axis of the test section under various flashing conditions and are reported herein.

The measured pressure distributions were combined with the centerline axial void fraction profiles to calculate the volumetric vapor generation rates under nonequilibrium conditions.

NRC Research and Technical  
Assistance Report

## TABLE OF CONTENTS

ABSTRACT . . . . .	i
LIST OF FIGURES . . . . .	iv
LIST OF TABLES . . . . .	viii
NOMENCLATURE . . . . .	ix
1. INTRODUCTION . . . . .	1
2. REVIEW OF LITERATURE . . . . .	2
3. EXPERIMENTAL TECHNIQUES . . . . .	4
3.1 Flow Loop . . . . .	4
3.2 Test Section . . . . .	6
3.3 Loop Operation Conditions and Instrumentation . . . . .	10
4. DATA ACQUISITION . . . . .	13
4.1 General Data Acquisition System . . . . .	13
4.2 Static Pressure Measurement Set-Up . . . . .	14
4.3 $\gamma$ -Densitometer for Void Fraction Measurements . . . . .	17
5. RESULTS AND DISCUSSION . . . . .	22
5.1 Single Phase Calibration . . . . .	22
5.2 Pressure Distributions Under Flashing Conditions . . . . .	28
5.2.1 Reproducibility Studies . . . . .	35
5.2.2 Operational Effects (Effect of Back Pressure) . . . . .	35
5.2.3 Parametric Effects . . . . .	39
5.2.4 Flashing Upstream of the Throat . . . . .	52
5.3 Void Fraction Measurements Under Flashing Conditions . . . . .	57
5.3.1 Flashing Close to the Throat . . . . .	57
5.3.2 Flashing Upstream of the Throat . . . . .	68
5.4 Calculations of Net Vapor Generation Rates Under Flashing Conditions . . . . .	71
6. SUMMARY AND CONCLUSIONS . . . . .	78
7. ACKNOWLEDGEMENTS . . . . .	80

TABLE OF CONTENTS (Cont'd)

8. REFERENCES . . . . .	82
NOTES TO THE APPENDICES . . . . .	84
Appendix A. Single Phase Calibration Data . . . . .	86
Appendix B. Pressure Distribution Data Under Flashing Conditions and Some Photographic Observations . . . . .	112
Appendix C. Pressure and Void Fraction Distributions Under Flashing Conditions . . . . .	156

## LIST OF FIGURES

### Figure

- 3.1 Schematic of BNL Heat Transfer Facility (BNL Neg. No. 1-1246-79).
- 3.2 Inside Dimensions of TS-2 (BNL Neg. No. 10-243-780)
- 3.3 Deviation From Design of TS-2 Inside Dimensions (BNL Neg. No. 10-244-78).
- 4.1 Schematic Representation of  $\gamma$ -Densitometer (BNL Neg. No. 3-1016-79)
- 4.2 Calibration of the Test Section Both Empty (Air) and Full of Water as a Function of Axial Distance (BNL Neg. No. 3-1018-79)
- 4.3 Calibration of the Test Section Both Empty (Air) and Full of Water as a Function of Radial Distance at a Fixed Axial Position (BNL Neg. No. 3-1020-79)
- 5.1 Typical Pressure Distributions Along TS-2 for the Single-Phase Flow Hydrodynamic Calibration Runs (BNL Neg. No. 3-1017-79)
- 5.2 Dimensionless Pressure Distribution for TS-2. Data is Averaged for all the Hydrodynamic Calibration Runs Performed (BNL Neg. No. 3-1022-79)
- 5.3 Typical Representation of an Isothermal Flashing Experiment in the p-T Diagram (BNL Neg. No. 3-1027-79)
- 5.4 Pressure Distributions Under Flashing and Nonflashing Conditions in TS-2 (BNL Neg. No. 3-1019-79)
- 5.5 Dimensionless Pressure Distributions in TS-2 Under Flashing Conditions as Compared to Single-Phase Hydrodynamic Calibration Data (BNL Neg. No. 3-1021-79)
- 5.6 Comparison of Pressure Distribution in Two Experiments to Show the Reproducibility of the Results at Low Mass Fluxes,  $G = 3.03 \text{ Mg/m}^2\text{s}$  (BNL Neg. No. 3-1029-79)
- 5.7 Comparison of Pressure Distributions in Two Experiments to Show Reproducibility of the Results at High Mass Flux,  $G = 4.45 \text{ Mg/m}^2\text{s}$  (BNL Neg. No. 3-1028-79)



LIST OF FIGURES (Cont'd)

Figure

- 5.8 Pressure Distributions Showing the Effect of Condensing Tank Back Pressure for Identical Nozzle Inlet Conditions (BNL Neg. No. 3-1031-79)
- 5.9 Photographic Observations for the Experimental Conditions Presented in Fig. (5.8). In these and all following photographs, the diameter of both the front and rear windows is 50 mm. (BNL Neg. No. 1-919-79).
- 5.10 Effect of Mass Flux on Pressure Distributions for Identical Nozzle Inlet Conditions Which are Close to the Onset of Flashing in the Test Section (BNL Neg. No. 3-1032-79).
- 5.11 Photographic Observations for the Experimental Conditions Presented in Fig. (5.10) (BNL Neg. No. 1-922-79).
- 5.12 Effect of Mass Flux on the Pressure Distributions in the Test Section (BNL Neg. No. 3-1033-79)
- 5.13 Photographic Observations for the Experimental Conditions Presented in Fig. (5.12) (BNL Neg. No. 1-918-79).
- 5.14 Effect of Nozzle Inlet Temperature at Constant  $(p_{in} - p_{sat}(T_{in}))$  on the Pressure Distribution in the Test Section (BNL Neg. No. 3-1030-79).
- 5.15 Photographic Observations for Experimental Conditions Presented in Fig. (5.14) (BNL Neg. No. 1-921-79).
- 5.16 Effect of Nozzle Inlet Temperature at Constant  $(p_{in} - p_{sat}(T_{in}))$  on the Pressure Distribution in the Nozzle (BNL Neg. No. 3-1037-79).
- 5.17 Effect of Nozzle Inlet Temperature at Constant  $(p_{in} - p_{sat}(T_{in}))$  on the Pressure Distribution in the Nozzle (BNL Neg. No. 3-1035-79).
- 5.18 Effect of Nozzle Inlet Temperature at Constant  $(p_{in} - p_{sat}(T_{in}))$  on the Pressure Distribution in the Nozzle (BNL Neg. No. 3-1034-79).
- 5.19 Photographic Observations for Experimental Conditions Presented in Fig. (5.16) and (5.18) (BNL Neg. No. 1-920-79).

LIST OF FIGURES (Cont'd)

Figure

- 5.20 Effect of Nozzle Inlet Pressure on the Pressure Distributions in the Test Section (BNL Neg. No. 3-1036-79)
- 5.21 Effect of Nozzle Inlet Pressure on the Pressure Distributions in the Test Section (BNL Neg. No. 3-1023-79)
- 5.22 Effect of Nozzle Inlet Pressure on the Pressure Distributions in the Test Section (BNL Neg. No. 3-1025-79)
- 5.23 Pressure Distributions in the Test Section While Flashing Onset is Upstream of the Nozzle Throat (BNL Neg. No. 3-1024-79)
- 5.24 Nondimensional Pressure Distribution  $DP^* = DP / \frac{1}{2} \rho U_0^2$  in the Test Section While the Flashing Onset is Upstream of the Nozzle Throat (BNL Neg. No. 3-1026-79)
- 5.25 Pressure and Axial Void Fraction Distributions in the Test Section. Plot of the difference between the dimensionless measured pressure drop and the non-dimensional pressure drop measured in the single phase calibration ( $DDP = DP_m^* - DP_c^*$ ) as a function of axial distance (BNL Neg. No. 3-1645-79).
- 5.26 Pressure and Axial Void fraction Distributions in the Test Section. Plot of the Difference Between the Dimensionless measured pressure drop and the non-dimensional pressure drop measured in the single phase calibration ( $DDP = DP_m^* - DP_c^*$ ) as a function of axial distance (BNL Neg. No. 3-1644-79).
- 5.27 Pressure and Axial Void Fraction Distributions in the Test Section. Plot of the difference between the dimensionless measured pressure drop and the non-dimensional pressure drop measured in the single phase calibration ( $DDP = DP_m^* - DP_c^*$ ) as a function of axial distance (BNL Neg. No. 3-1643-79).

LIST OF FIGURES (Cont'd)

Figure

- 5.28 Pressure and Axial Void Fraction Distributions in the Test Section. Plot of the difference between the dimensionless measured pressure drop and the non-dimensional pressure drop measured in the single phase calibration ( $DDP = DP_m^* - DP_c^*$ ) as a function of axial distance (BNL Neg. No. 3-1642-79).
- 5.29 Pressure and Axial Void Fraction Distributions in the Test Section. Plot of the difference between the dimensionless measured pressure drop and the non-dimensional pressure drop measured in the single phase calibration ( $DDP = DP_m^* - DP_c^*$ ) as a function of axial distance (BNL Neg. No. 3-1110-79).
- 5.30 Pressure and Axial Void Fraction Distributions in the Test Section. Plot of the difference between the dimensionless measured pressure drop and the non-dimensional pressure drop measured in the single phase calibration ( $DDP = DP_m^* - DP_c^*$ ) as a function of axial distance (BNL Neg. No. 3-1111-79).
- 5.31 Pressure and Axial Void Fraction Distributions in the Test Section. Plot of the difference between the dimensionless measured pressure drop and the non-dimensional pressure drop measured in the single phase calibration ( $DDP = DP_m^* - DP_c^*$ ) as a function of axial distance (BNL Neg. No. 3-1112-79).
- 5.32 Pressure and Axial Void Fraction Distributions in the Test Section With Flashing Occurring Upstream of the Nozzle Throat. Plot of the Difference Between the Dimensionless Measured Pressure Drop and the Nondimensional Pressure Drop Measured in the Single Phase Calibration, ( $DDP = DP_m^* - DP_c^*$ ) as a Function of Axial Distance. (BNL Neg. No. 3-1108-79).
- 5.33 Pressure and Axial Void Fraction Distributions in the Test Section With Flashing Occurring Upstream of the Nozzle Throat. Plot of the Difference Between the Dimensionless Measured Pressure Drop and the Nondimensional Pressure Drop Measured in the Single Phase Calibration, ( $DDP = DP_m^* - DP_c^*$ ) as a Function of Axial Distance. (BNL Neg. No. 3-1109-79).

575 029

LIST OF FIGURES (Cont'd)

Figure

- 5.34 Top: Measured Pressure (o) and Void Fraction (□) Distributions in the Converging Part of the Test Section in Runs 82/821 and the Least Square Polynomial Fit to Data.
- Bottom: Calculated Net Vapor Generation Rate Based on the Least Square Fit to the  $\alpha$  and  $p$  Data. (BNL Neg. No. 3-1226-79).
- 5.35 Top: Measured Pressure (o) and Void Fraction (□) Distributions in the Converging Part of the Test Section in Runs 83/832 and the Least-Square Polynomial Fit to the Data.
- Bottom: Calculated Net Vapor Generation Rate Based on the Least-Square Fit to the  $\alpha$  and  $p$  Data. (BNL Neg. No. 3-1225-79).

LIST OF TABLES

- TABLE I Operational Range of the Facility
- TABLE II Test Section Instrumentation
- TABLE III Typical Pressure Drop Data
- TABLE IV Calibration Data for the Test Section Both Empty (Air),  $I_E$ , and Full of Water,  $I_F$  (Date 1-19-79)
- TABLE V Summary of Experimental Conditions
- A. Hot and Cold Calibration
- B. Flashing Experiments
- TABLE VI Void Fraction Distribution Data

## NOMENCLATURE

$A, A^+$	nozzle cross sectional area, and throat area, respectively
$C_o$	distribution parameter
$D$	diameter
$DP$	pressure differential between the test section inlet (tap 1) and a specific tap location along the nozzle. (This difference does not include any gravitational head effects.)
$DP^*$	$= DP / \frac{1}{2} \rho U_o^2$ , dimensionless pressure differential
$DPP$	$= DP_m^* - DP_c^*$
$G$	mass flux
$g$	acceleration of gravity
$I_E$	number of counts for a specific period of time at a given location while the test section is empty (full of air)
$I_F$	number of counts for a specific period of time at a given location while the test section is full of water
$I_{2\phi}$	number of counts for a specific period of time at a given location under two-phase conditions
$j$	volumetric flux
$L$	axial length
$p$	pressure
$R$	radial coordinate
$T$	temperature
$U_o$	test section inlet velocity $= G / A_{in} \rho_{in}$
$u$	velocity
$V_{gj}$	drift velocity of vapor
$x$	quality
$Z$	axial coordinate along the nozzle

NOMENCLATURE (Cont'd)

$\alpha$	void fraction
$\Gamma_v$	mass of vapor generated per unit time per unit volume of mixture
$\rho$	density
$\mu$	$\gamma$ attenuation coefficient
$\sigma$	surface tension

Subscripts

none	mixture
c	single phase calibration
ct	condensing tank (test section discharge)
f	saturated liquid
g	saturated vapor
in	test section inlet
l	liquid
m	measured
sat	saturation
v	vapor

Superscript

*	dimensionless
---	---------------

Symbol

< >	area averaged quantity
-----	------------------------

## 1. INTRODUCTION

Several experimental, as well as analytical investigations have been undertaken to date in order to calculate the discharge flow rates of two-phase mixtures from pipes, nozzles, and orifices accurately. This problem presents itself in the safety analysis of water cooled nuclear reactors and also in the safe storage and handling of liquid cryogens in space applications.

During a hypothetical Loss-Of-Coolant Accident (LOCA) of a nuclear reactor, the flow is expected to be choked at the break. The discharge flow rate affects the heat transfer in the core, the depressurization rate of the containment vessel, and it dictates the design requirements of the Emergency Core Cooling System (ECCS). Theoretical models have been proposed, and large computer codes have been developed, to predict the critical flow rates and their dependence on the upstream thermodynamic and flow conditions, as well as the pipe size and component geometry. At present, there is no general model or correlation for critical flows which considers both thermal nonequilibrium and relative velocities between the phases and which is valid for a wide range of pipe lengths, diameters, and upstream conditions, including subcooled liquid. A modeling effort in conjunction with well-controlled experiments is currently being undertaken at Brookhaven National Laboratory to investigate and measure the actual vapor generation rates under nonequilibrium conditions. The purpose of this report is to describe the test facility, including the venturi test section and loop instrumentation, as well as to present the experimental results and photographic observations acquired to date under nonequilibrium flashing conditions.

575 033

## 2. REVIEW OF THE LITERATURE

Extensive analytical and experimental work has been reported on the two-phase critical flows in the last three decades. Thorough reviews have been presented by Hsu (1972) and Saha (1978). The latter summarized the various available critical flow models and emphasized the effects of thermal nonequilibrium and relative velocities between the phases, which become prominent under certain conditions. Since the objective of the present research was the determination of the vapor generation rates under nonequilibrium conditions, we will concentrate on pertinent experimental work in the literature.

To study flashing flows and critical flow conditions, researchers have used several kinds of test facilities. Some use an upstream vessel containing a saturated or subcooled liquid, which expands and may vaporize in the test section. Others have used systems where the two phases are generated separately and then mixed together before being introduced into the test section. When either system is operated as a once-through experiment, the flow from the test section discharges into a downstream container whose pressure can be adjusted independently of the upstream conditions. When either system is operated as a steady closed loop, the control of the downstream pressure independently of the upstream conditions becomes more difficult to achieve due to the hydrodynamic coupling of the test section with the loop. In this report, we will consider only experiments conducted with subcooled or saturated inlet conditions. The various test sections investigated to date can be classified as: first, long tubes and nozzles; second, short tubes and short nozzles; and third, orifices.



Long tubes and nozzles can be characterized by  $L/D > 40$  (Seynhaeve 1977). Such experiments were conducted by Isbin, Moy, and DaCruz (1957), James (1962), Fauske (1965), Reocreux and Seynhaeve (1974), Ardron and Ackerman (1978), etc. Reocreux (1974) was the first researcher to provide pressure measurements, as well as void fraction distributions which allow the direct calculation of the vapor generation rates, provided a specific slip model is adopted. In all of the experiments conducted with long straight pipes, the frictional effects are equally important as the vapor generation rate to the choking condition, and thus the vapor generation effect can not be singled out easily.

Short tubes and nozzles with  $1 < L/D < 40$  have been extensively investigated by Silver (1948), Zaloudek (1963), Fauske and Henry (1971), and Schrock, Strickman and Brown (1977). Similar choked flow experiments were also reported by Simoneau (1975) and Hendrick, Simoneau, and Barrows (1976) with cryogenic liquids. Although the experiments in this group with a converging diverging nozzle can provide information on the flashing inception, and choking conditions, no detailed void fraction measurements were performed to allow the determination of vapor generation rates in any of the experiments in the literature.

Experiments with orifices were usually conducted using orifices with  $L/D < 1$  placed in a uniform cross section tube, and the jet has been investigated by several authors. More recently, Seynhaeve (1977) measured axial and radial void fractions of the jet, in addition to the pressure distributions.

### 3. EXPERIMENTAL TECHNIQUES

#### 3.1. Flow Loop

The main flow loop presented in Fig. (3.1) is constructed from "three inch" nominal (7.6 cm) stainless steel pipe. High purity water is circulated through the loop using a centrifugal pump rated at 1500  $\ell$ /min at a head of 600 kPa.

Starting from the pump, the fluid passes through a flow control station where the flow rate can be controlled from 3 to 950  $\ell$ /min and measured with an accuracy of 1/2 percent of full scale. Excess flow from the pump is directed to secondary loops for cooling, purification and simple bypass flow routing. After the flow rate is set and measured, the fluid passes through the heater system where up to 520 kW of heat can be added to the water, and the outlet temperature can be regulated to  $\pm 0.3^\circ\text{C}$  over the entire controlled flow range.

Leaving the heater system, the fluid passes through the test section. A pressurizer is connected to the main loop between the heater system and the test section and, when valved in, the pressurizer fixes the inlet pressure to the test section. Alternately, the pressurizer may be isolated from the loop and in this fashion, the pressure in the loop is controlled by pump flow rate. Thus, two modes of operation are possible: the pressure controlled and the flow controlled modes. Once the fluid has passed through the test section, it enters a condensing tank where a cooling spray is utilized to condense the vapor and to fix the tank temperature. Since the pressure in the tank is essentially the same as in the test section exit,

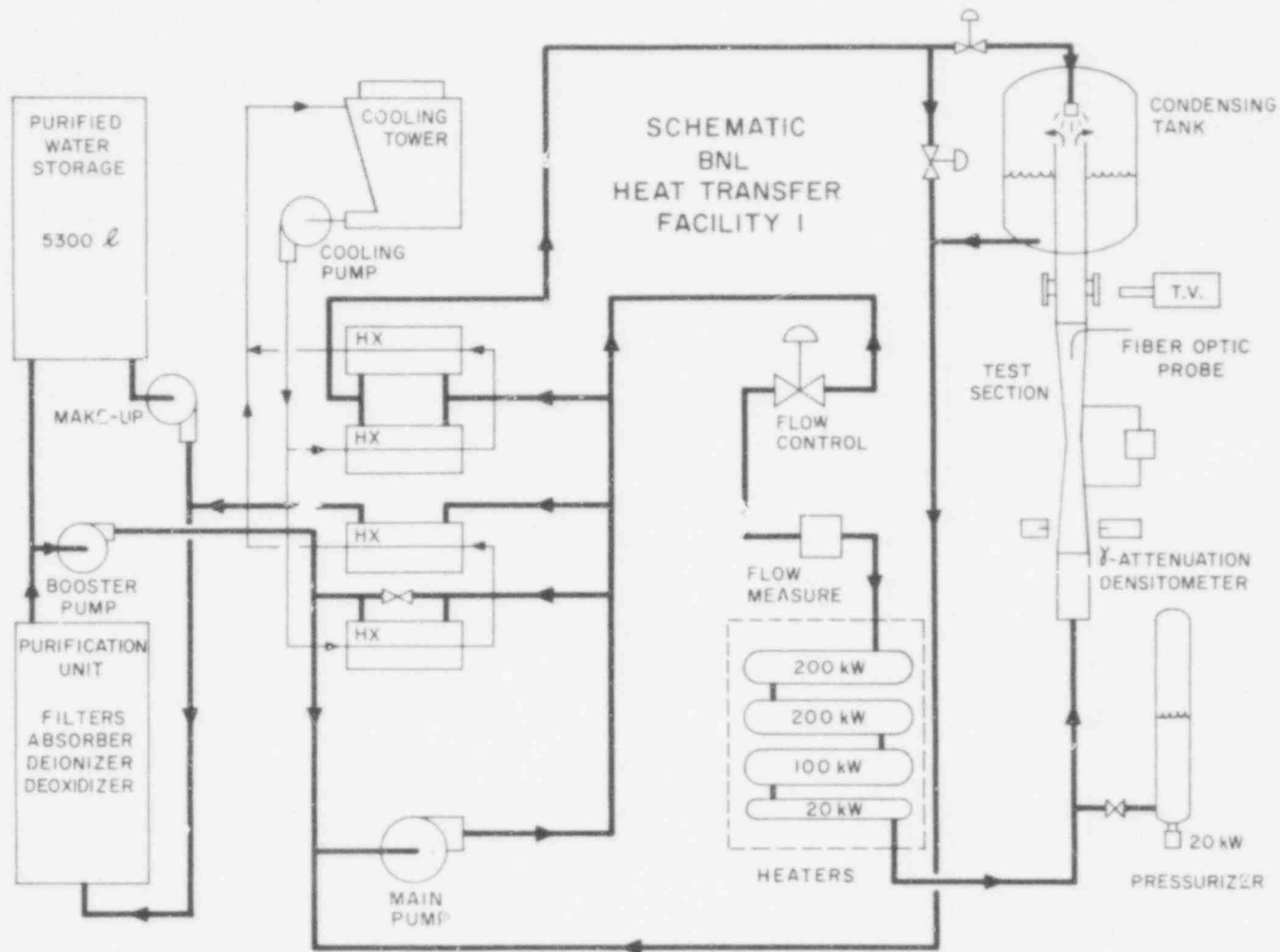


Figure 3.1 Schematic of BNL Heat Transfer Facility (BNL Neg. No. 1-1246-79).

the condensing tank and pressurizer can be used together to fix the pressure drop across the test section.

The fluid travels, after leaving the condensing tank, back to the pump, and, depending on conditions, cooling water can be added to this flow to prevent cavitation in the pump. Cooling water is provided from excess pump flow and is cooled by shell and tube heat exchangers tied to a 730 kW cooling tower.

Purification of the test fluid is accomplished during initial filling of the test loop. The water is deoxidized, deionized and passed through 0.22 micron filters. In addition, about 40 l/min of excess pump flow is passed through the purification station as a polishing procedure during flow loop operation.

### 3.2. Test Section

The test section is made of stainless steel with a total length of 78.7 cm, including a symmetrical converging/diverging portion of 55.9 cm length and inside diameters of 5.1 cm at the ends and 2.5 cm at the throat. The wall thickness varies only from 0.57 mm to 0.60 mm over the entire tube length. "Intrimiks" were used to accurately map the interior dimension of TS-2. The data taken have been reduced and analyzed and are summarized in Figs. (3.2) and (3.3). A reference datum was established as the flange face on the inlet to the test section assembly. Figure (3.2) shows the mean inside diameter plotted as a function of the axial distance from the reference datum. Each point is the mean of four measurements made at a particular axial distance with the "intrimik" rotated  $90^{\circ}$  in each case. The

-7-  
575 039

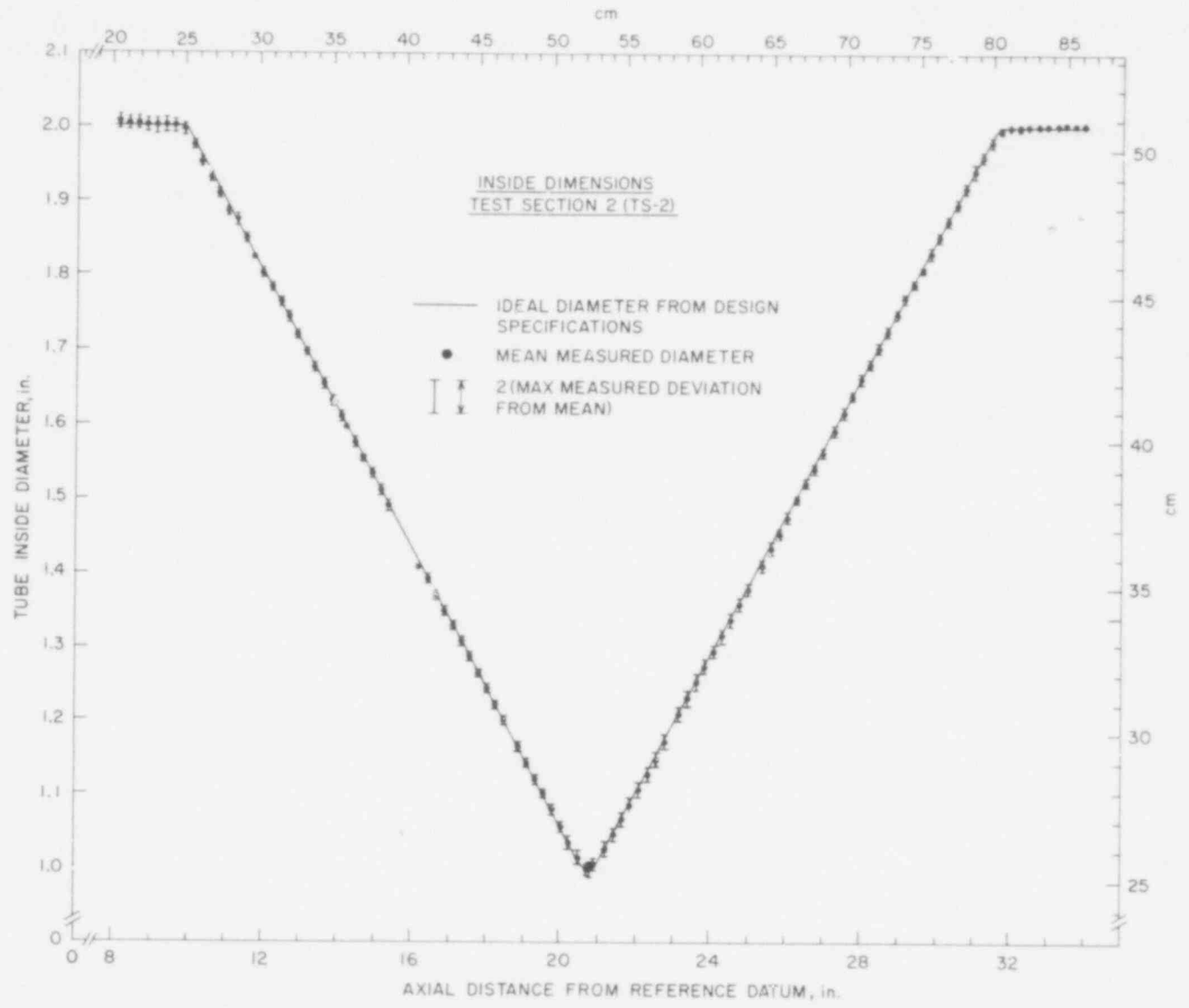


Figure 3.2 Inside Dimensions of TS-2 (BNL Neg. No. 10-243-780)

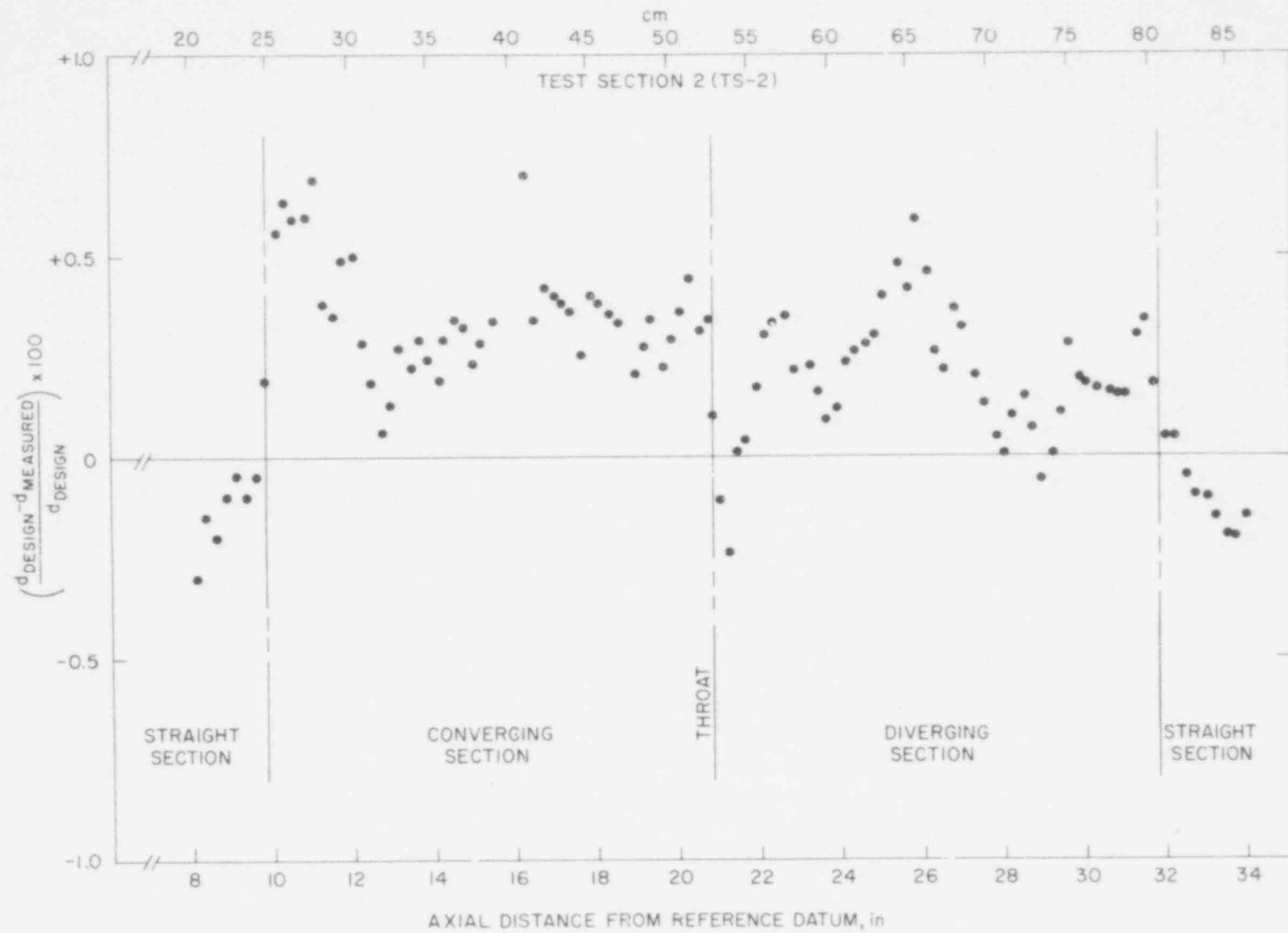


Figure 3.3 Deviation From Design of TS-2 Inside Dimensions (BNL Neg. No. 10-244-78).

575 040

"error bars" show the maximum deviation from the mean encountered at each point. The solid line plotted is the actual design dimensions for the test section that were specified prior to construction. A point by point comparison of the design versus the measured dimensions is given in Fig. (3.3), and shows that most of the measured dimensions deviate less than one-half a percent from the design.

The test section design and construction was performed in three levels, each with an increased complexity in instrumentation. In the first level, 49 wall pressure taps (0.4 mm in diameter) were installed on 1.27 cm center along the length of the venturi, in addition to a set of observation windows located 30 cm downstream of the test section exit, which allowed photographic observations by flash photography. Taps 1, 2, and 3 are in the constant area entrance of the converging section, while Taps 47, 48, and 49 are at the exit of the diverging section. If we take Tap 1 as the origin of the axial coordinate, as designed, Tap 25 is located 30.61 cm downstream. However, as constructed, the throat determined from the actual diameter measurements reported above is located at 30.48 cm downstream of Tap 1. This fact implies that Tap 25 is 0.13 cm downstream of the geometric throat. An additional pressure tap, 50, is located at 159 cm upstream of the test section inlet tap 1. The gauge pressure at Tap 50, with respect to the atmospheric pressure, is constantly monitored at the control panel, and it provides the needed information to calculate the absolute pressure at the test section inlet within an accuracy of  $< 1$  percent. The temperature is monitored by means of two platinum resistance thermometers, one located near pressure Tap 50 for the flow inlet conditions and one at the condensing tank for the flow outlet conditions.

In the second level, a single channel (i.e., single beam) gamma densitometer which can be traversed virtually everywhere within the test section was added for chordal averaged void fraction measurements. As the system develops, the single beam densitometer will be replaced by two banks of five beams each for more efficient data taking and cross correlation. A stationary hydrofoil-like probe containing ten pairs of local sensors is planned to be the third level of construction, and it will allow the measurement of local void fractions and phase velocities across a particular diameter.

To date, pressure distribution, as well as void fraction distribution data have been taken, and the flashing regimes were recorded photographically by means of a flash and a still camera arrangement located downstream of the test section outlet.

### 3.3. Loop Operation Conditions and Instrumentation

The operational range of the facility is summarized in Table I. The inlet pressure and temperature can be varied from 100-1000 kPa and from room temperature to 150°C respectively. The inlet mass flux covers a range of 1.1-7.9 Mg/m<sup>2</sup>s. These operation limits cover an approximate Reynolds number range of 10<sup>5</sup>-10<sup>6</sup> based on test section inlet conditions. The various loop instrumentation, including ranges and accuracies, are tabulated in Table II. Pressure measurements are accomplished by means of Statham gauges, each calibrated to an accuracy better than 0.1 percent of the reading. The temperatures are measured by thermocouples and RTD's, and the flow rate measurements are obtained by two Cox turbine flow meters, upstream of the test section in the subcooled flow region.



TABLE I

## OPERATIONAL RANGE OF THE FACILITY

Test Section Inlet Pressure	100 - 1000 kPa
Test Section Inlet Temperature	20 - 150°C
Mass Flux	1.1 - 7.9 Mg/m <sup>2</sup> s
Reynolds Number Based on Inlet Conditions	10 <sup>5</sup> - 10 <sup>6</sup>

Converging Test Section Inlet Conditions From  
Subcooled To Low Qualities

TABLE II

## TEST SECTION INSTRUMENTATION

QUALITY MEASURED	TYPE OF SENSOR	RANGE	ACCURACY
Temperature	Resistance Temp. Detector (RTD)	-200 to 500°C	1.2% @ 200°C
Differential Pressure	Strain Gage $\Delta p$ Transducer	4 to 500 kPa	1% of Reading
Flow Rate	Turbine Meter	3 to 950 l/min	0.5% Full Scale
Void Fraction	Gamma Densitometer (Thulium/Cad-Telluride)	0 to 1	5% Steady State (Future 5% per 1 ms)

#### 4. DATA ACQUISITION

##### 4.1 General Data Acquisition System

The centralized Data Acquisition and Data Analysis System (DADAS) was designed as a real time digital data system with multiterminal multitasking capability. The system was constructed around a Hewlett Packard 9640 system consisting of a 21MX minicomputer with 112 kilowords of central memory, 7.5 megaword cartridge discs, 9 track magnetic tape transport and paper tape I/O. Central control of the system is accomplished with a CRT terminal while the 3 satellite stations employ silent 700 terminals. Tabular and graphical presentation of data is achieved with a Varian electrostatic printer/plotter capable of listing 600 LPM and plotting 1.6 ips. Interface of the ADC systems is both direct, an interface per device, and via the universal interface bus, IEEE standard 488.

Three levels of ADC speed and resolution are incorporated within DADAS. The slow speed, high resolution system employs an integrating digital voltmeter with microvolt resolution and 300 channel guarded crossbar scanner. The through-put rate of this system is up to 18 measurements per second with high common mode voltage rejection capability. The intermediate speed system is a 15 bit ( $\pm 10.24$  volts) multiplexed ADC with a 50 kHz through-put rate. The system employs a single programmable gain amplifier and a signal conditioning amplifier and filter per channel. The system has high common mode voltage rejection capability and can be connected directly to experiments. The high speed system is also a 15 bit ( $\pm 10.24$  volt) multiplexed ADC with a 500 kHz through-put rate. The system has eight input

channels with simultaneous sample and hold amplifiers. This system was designed specifically for digitizing analog tapes.

#### 4.2. Static Pressure Measurement Set-Up

Each of the 49 pressure taps on the test section can be connected to either of two manifolds, one a common high side the other a common low side, via two hand operated toggle valves to the low or high pressure sides of a pressure transducer bank. The differential pressure between two locations along the test section can be measured by connecting the two taps to the low and high sides of the pressure transducer. Six Statham pressure transducers with the ranges of 17, 34, 69, 170, 340, and 690 kPa (2.5, 5, 10, 25, 50, 100 psi) were connected in parallel to the two pressure measuring manifolds through two solenoid valves. A third solenoid valve in each transducer allows the shorting of the high and low pressure lines and thus provides a means of measuring and monitoring the zero point stability of the transducer preceding every  $\Delta p$  measurement. The solenoid valves are designed for a 200 psi differential pressure and were tested prior to installation. Once the two pressure taps were manually connected to the high and low pressure manifolds, the computer controlled procedure described below was initiated for the recording of the data.

Each measurement started with the pressure gauge shorted to record the zero  $\Delta p$  output. The pressure differential between the two taps was then measured across the 690 kPa (100 psi) range transducer. Once the pressure differential was calculated, the system automatically selected a pressure transducer such that the DP to be measured would fall between 25 and 75

percent of the full range of the particular transducer chosen. With the chosen transducer, the computer first measured the gauge's zero output when shorted, then took 20 consecutive DP readings, averaged them, and calculated their standard deviation. The same sequence was repeated once again and the new average of 20 new readings was compared to the last one calculated. If the two consecutive averages were within one percent of each other, the measurement was accepted and printed out as a data point. At the same time, the instantaneous flow rate and other flow variables of interest were also recorded. On the other hand, if the two consecutive averages did not satisfy the acceptance criterion, the computer repeated this procedure until the criterion was met or until 15 sets of 20 readings each were made and the last output was printed as the data point. This procedure permitted the measurement of static pressures with an accuracy of 1 percent of the reading as quoted in Table II. It also allowed us to detect the presence of large pressure fluctuations at the onset of flashing or condensation. At other locations, such fluctuations were not observed and the readings converged smoothly. It should be noted that since the pressure transducers were located at the same horizontal level, gravity effects due to the elevation difference of the pressure taps were canceled out in the measurements. The pressure data reported here represent the difference, at two pressure taps, of the sum of the static pressure and gravitational head. A typical output for an experiment is presented in Table III, which depicts the data acquisition format with the tap identity, pressure data, as well as various other instantaneous flow parameters of interest.

TABLE III

## TYPICAL PRESSURE DROP DATA

BNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER 74

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLES
1-3	10.36	96.3	99.3	87.9	285.9	55.5	510.4	.865E+06	.00	.00
1-5	10.35	96.3	99.3	87.9	284.7	55.5	509.8	.864E+06	2.38	.12
1-7	10.39	96.3	99.4	88.0	284.5	55.4	511.6	.867E+06	6.21	.49
1-9	10.37	96.3	99.3	87.8	283.8	55.4	510.6	.866E+06	10.95	.87
1-11	10.39	96.3	99.3	87.8	284.6	55.5	511.4	.867E+06	18.39	1.45
1-13	10.36	96.3	99.4	87.9	284.8	55.5	510.3	.865E+06	26.64	2.12
1-15	10.38	96.3	99.3	87.9	284.7	55.5	511.2	.866E+06	36.44	2.89
1-17	10.37	96.3	99.4	87.7	284.0	55.5	510.7	.866E+06	56.23	4.46
1-19	10.36	96.3	99.4	87.6	283.8	55.6	510.1	.865E+06	73.37	5.84
1-20	10.36	96.3	99.4	87.9	284.2	55.6	510.1	.865E+06	87.11	6.93
1-21	10.39	96.3	99.3	87.8	284.4	55.6	511.5	.867E+06	104.25	8.25
1-22	10.36	96.3	99.3	87.9	284.6	55.6	510.3	.865E+06	127.88	10.16
1-23	10.38	96.3	99.3	87.8	285.2	55.6	511.3	.867E+06	147.31	11.66
1-24	10.36	96.3	99.3	87.8	284.0	55.6	510.3	.865E+06	176.15	14.00
1-25	10.36	96.3	99.4	87.6	283.5	55.6	510.0	.865E+06	208.24	16.57
1-26	10.34	96.3	99.3	87.6	284.8	55.8	509.2	.863E+06	196.18	15.66
1-27	10.39	96.3	99.3	87.9	285.4	55.8	511.5	.867E+06	195.73	15.48
1-28	10.37	96.3	99.3	87.8	285.5	55.7	510.5	.865E+06	196.05	15.57
1-29	10.37	96.3	99.3	87.8	285.8	55.8	510.7	.866E+06	195.34	15.50
1-31	10.39	96.3	99.3	87.7	283.8	55.8	511.7	.867E+06	194.48	15.37
1-33	10.39	96.3	99.3	87.9	284.0	55.7	511.4	.867E+06	194.10	15.36
1-35	10.35	96.3	99.3	88.0	284.8	55.7	509.9	.864E+06	193.55	15.41
1-37	10.38	96.3	99.3	88.2	285.2	55.7	511.0	.866E+06	193.37	15.33
1-39	10.38	96.3	99.4	88.1	285.7	55.7	510.9	.866E+06	192.95	15.30
1-41	10.34	96.3	99.3	87.8	284.0	55.7	509.4	.863E+06	192.72	15.37
1-43	10.38	96.3	99.3	87.8	284.4	55.7	511.1	.866E+06	192.72	15.27
1-45	10.38	96.3	99.3	88.1	284.6	55.7	511.2	.866E+06	191.99	15.20
1-47	10.35	96.3	99.3	87.8	283.6	55.8	509.7	.864E+06	191.92	15.29
1-49	10.39	96.3	99.3	88.2	284.6	55.7	511.6	.867E+06	192.15	15.19
50-1	10.37	96.3	99.3	88.1	284.5	55.5	510.5	.865E+06	17.94	1.42

575  
048

#### 4.3. $\gamma$ -Densitometer for Void Fraction Measurements

The single channel  $\gamma$  densitometer set up presented in Fig. (4.1) was used for the void fraction measurements. Thulium-170, obtained as 99.999 percent pure Thulium Oxide powder, sealed in an aluminum cylinder formed the basic material of the  $\gamma$ -source. The present source was purchased from Amersham Corporation and was irradiated at the High Flux Beam Reactor at Brookhaven National Laboratory. The source strength was kept at a few millicuries due to the presence of high energy-activity (1.12 MeV), which is due to trace amounts ( $\sim 70$  ppm) of Scandium impurity present in the source material and which caused difficulties from the Health Physics and Safety point-of-view. The source capsule is placed in a "lead pig," with a collimator opening of 2.5 mm in diameter, which determines the size of the  $\gamma$  beam. The detector consisted of a Cadmium Telluride crystal (2.5 x 2.5 mm) mounted on a regular BNC connector. The CdTe detector was connected to "off-the-shelf" radiation electronic components (Tennelec), consisting of a preamplifier (TC 164), a high voltage power supply (TC 948) for the bias voltage (150 V), a linear amplifier (TC 203 BLR), a single channel analyzer (TC 440), a T 541 Timer and a scaler (TC 540A). The single channel analyzer was used in the differential discriminator mode of operation and the energy window was set around 84 keV with a dispersion range of  $\pm 10$  keV. The TC 541 timer was altered by Tennelec to include time intervals as short as 0.1 msec and as long as 54 sec. The  $\gamma$  source holder and detector were set on a traversing mechanism, which allowed both axial and radial traverses along the test section. The axial and radial repositioning of the  $\gamma$  beam by the traversing mechanism can be accomplished with an accuracy of  $\pm 0.05$  mm.

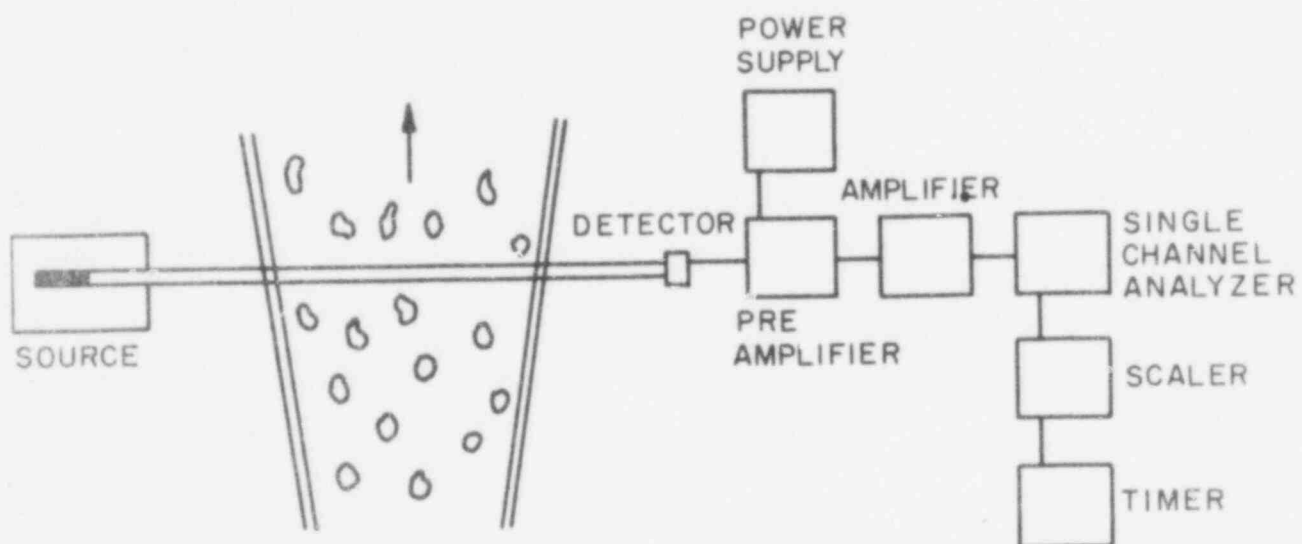


Figure 4.1 Schematic Representation of  $\gamma$ -Densitometer  
(BNL Neg. No. 3-1016-79)



The chordal averaged void fraction were calculated from the following relation:

$$\alpha = 1 - \frac{\rho_{\ell m}}{\rho_{\ell c}} \frac{\ln \frac{I_{2\phi}}{I_E}}{\ln \frac{I_F}{I_E}} \quad (1)$$

where  $\alpha$  is the chordal-averaged void fraction,  $I_E$ , and  $I_F$  are the number of counts during a preset period of time when the test section is "empty", i.e., full of air (attenuation due to stainless steel walls only) and full of water respectively, and  $I_{2\phi}$ , is the number of counts during the same preset period of time under two-phase flow conditions.  $\rho_{\ell c}$  is the water density at the calibration temperature, (20°C) and  $\rho_{\ell m}$  is the water density at the temperature where the experiment was being conducted.

The calibration of the test section along the axis was performed with the test section empty and full of water at 20°C (Table IV). Figure (4.2) presents the calibration data, as well as the calculated values (solid squares) derived from the physical measurements of wall thickness and inside diameter along the nozzle. For these calculations, the attenuation coefficients for steel was taken as  $\mu_{st} = 2.7 \text{ cm}^{-1}$  and for water  $\mu_w = 0.167 \text{ cm}^{-1}$ , both values are listed for a 100 keV  $\gamma$ -energy level (Reactor Physics Constants, 1963). All calculated values were normalized to the entrance of the nozzle when the test section was empty, which provided a value of  $I_0 = 2854 \text{ c/54 s}$ . The calibrations were also repeated on different days, and the repeatability of the results are satisfactory, as long as the source decay is taken into consideration. Radial calibration data were recorded at a given axial location ( $Z = 183 \text{ mm}$ ) and are presented in Fig.

TABLE IV

CALIBRATION OF THE TEST SECTION BOTH EMPTY (AIR),  $I_E$ ,  
AND FULL OF WATER,  $I_F$ . (Date 1-19-79)

AXIAL LOCATION Z(mm)	$I_F$ counts/54s	$I_E$ counts/54s	AXIAL LOCATION Z(mm)	$I_F$ counts/54s	$I_E$ counts/54s
5.1	941	2045	304.8	1239	1856
30.5	964	2053	307.2	1286	1944
55.7	976	1994	309.8	1307	2061
81.3	1019	2027	312.3	1360	2188
106.7	1017	1974	314.8	1371	2122
132.1	1110	2047	317.6	1374	2165
157.4	1125	2035	319.9	1396	2161
182.9	1147	2009	322.5	1419	2220
208.1	1206	2021	325.2	1427	2199
233.7	1260	2031	327.7	1406	2189
259.1	1260	1989	330.2	1354	2155
271.8	1328	2060	332.6	1337	2077
274.3	1337	2062	335.1	1280	2076
276.9	1341	2059	360.8	1210	2025
279.4	1313	2039	386.0	1146	2019
281.9	1338	2031	411.4	1180	2044
284.4	1352	2061	436.8	1113	2013
287.0	1366	2071	462.3	1081	1989
289.5	1378	2101	488.6	1039	2002
292.0	1367	2027	513.1	1003	2011
294.5	1355	2063	538.5	1009	2038
297.1	1338	2009	563.8	957	2082
299.6	1318	1986	576.5	961	2078
302.2	1278	1932			

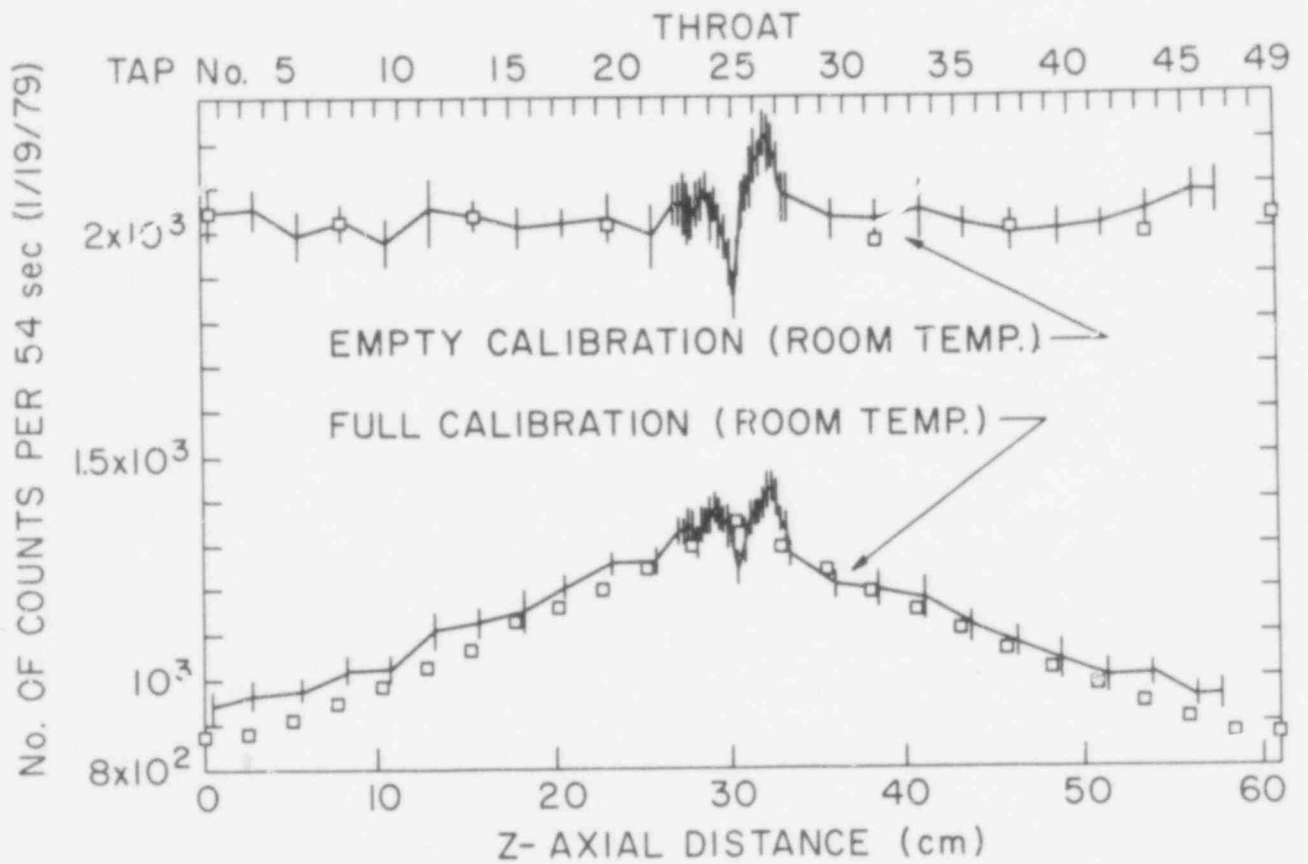


Figure 4.2 Calibration of the Test Section Both Empty (Air) and Full of Water as a Function of Axial Distance (BNL Neg. No. 3-1018-79)

575 053

(4.3). The circles at  $R = 0$ , which is the axial location, corresponds to the calibration measurements reported in Fig. 4.2 at  $Z = 183$  mm. The reproducibility of the results is very good.

In Figs. (4.2) and (4.3), the bars present the standard deviations of ten consecutive measurements. The accuracy of the system ( $\sim 4$  percent) is still governed by the statistical error  $\frac{dI}{I} = \frac{1}{\sqrt{I}}$ , due to the low rate of counts which in turn is caused by the low source activity. Increasing the source strength to higher activity level should improve the statistical errors by increasing the number of counts per second.

## 5. RESULTS AND DISCUSSION

In this section, results will be presented for the single phase nozzle calibration experiments, as well as pressure and void fraction distributions and photographic observations under various flashing regimes. All the experiments reported herein are tabulated in Table V with their respective inlet conditions, mass flux and corresponding condensing tank conditions.

### 5.1. Single Phase Calibration

The hydrodynamic calibration of the test section was done to determine the performance characteristics under single phase flow conditions and to obtain the axial distribution of the effective nozzle cross-sectional area.

Three main parameters were varied during these calibration tests: the mass flux ( $1.6-7.9 \text{ Mg/m}^2\text{sec}$ ), the inlet pressure (300-1000 kPa), and the inlet temperature ( $23-149^\circ\text{C}$ ). These experiments covered Reynolds numbers



Figure 4.3 Calibration of the Test Section Both Empty (Air) and Full of Water as a Function of Radial Distance at a Fixed Axial Position (BNL Neg. No. 3-1020-79)

TABLE V

## SUMMARY OF EXPERIMENTAL CONDITIONS

## A. COLD &amp; HOT CALIBRATION

RUN	$P_{in}$ (kPa)	$T_{in}$ ( $^{\circ}$ C)	$G$ ( $Mg/m^2s$ )	$P_{ct}$ (kPa)	$T_{ct}$ ( $^{\circ}$ C)
1	-----	-----	----	---	-----
2	371	26.4	1.56	354	26.3
3	368	26.8	3.13	345	26.2
4	361	27.2	4.71	331	26.6
5	351	27.6	6.28	311	27.4
6	682	27.7	7.01	647	27.2
7	691	27.3	6.30	657	27.3
8	695	26.9	4.71	652	26.8
9	709	27.1	3.13	674	26.6
10	711	27.0	1.56	683	27.0
11	688	27.7	6.26	632	27.6
12	1033	29.2	7.01	973	29.1
13	1031	29.4	7.88	961	29.3
14	337	23.0	6.25	316	22.9
15	348	22.9	4.74	339	22.9
16	365	66.3	3.08	309	66.1
17	367	64.1	1.56	322	63.9
18	-----	-----	----	---	-----
19	337	94.4	5.49	324	94.5
20	337	11.6	4.71	352	12.
21	315	11.9	6.29	326	11.9
22	336	12.3	3.15	369	12.3
23	293	69.1	3.08	308	68.9
24	692	148.4	2.33	646	148.4
25	213	54.0	3.35	201	48.6
26	211	54.4	3.34	203	48.8

B. FLASHING EXPERIMENTS

RUN	$P_{in}$ (kPa)	$T_{in}$ ( $^{\circ}$ C)	$G$ (Mg/m <sup>2</sup> s)	$P_{ct}$ (kPa)	$T_{ct}$ ( $^{\circ}$ C)
20	281.	98.3	4.90	245.	98.2
21	393.	100.6	6.01	136.	100.4
22	170.	100.2	3.04	125.	100.1
23	130.	99.4	1.81	121.	99.3
24	160.	98.0	3.05	122.	97.8
25	247.	97.4	4.52	125.	97.3
26	386.	97.8	6.02	132.	97.7
27	326.	130.0	2.95	299.	129.6
28	566.	131.7	5.90	316.	131.4
29	488.	123.5	5.77	210.	115.4
30	375.	125.1	4.50	206.	114.7
31	----	-----	----	----	-----
35	287.	99.4	4.96	250.	99.2
37	296.	100.3	4.94	170.	100.0
38	117.	100.3	2.05	112.	99.8
39	136.	100.5	2.25	112.	100.1
40	168.	100.3	3.02	112.	100.0
41	250.	100.2	4.54	115.	99.8
42	194.	99.6	3.79	114.	99.4
43	287.	100.2	4.97	121.	99.9
44	271.	99.9	4.50	101.	99.9
45	308.	99.8	4.97	99.	100.0
46	223.	99.9	3.79	99.	99.9
47	----	-----	---	----	-----

B. FLASHING EXPERIMENTS

(Cont'd)

RUN	$p_{in}$ (kPa)	$T_{in}$ ( $^{\circ}$ C)	$G$ (Mg/m <sup>2</sup> s)	$p_{ct}$ (kPa)	$T_{ct}$ ( $^{\circ}$ C)
48	183.	99.9	3.04	100	99.9
49	146.	99.9	2.27	99	99.7
50	142.	99.8	2.04	101	99.9
51	----	-----	----	---	-----
52	381.	123.5	4.48	254	123.5
53	395.	123.6	4.45	249	123.6
54	525.	123.6	5.96	252	123.7
55	293.	123.6	2.99	251	123.6
56	261.	123.2	2.20	252	123.6
57	263.	124.7	2.04	256	123.9
58	254.	123.3	2.98	174	110.2
59	254.	123.1	2.98	174	110.2
60	264.	125.8	2.93	186	112.5
61	259.	123.8	2.98	162	108.8
63	739.	148.7	5.85	464	148.7
64	609.	148.8	4.40	463	148.8
65	----	-----	----	---	-----
66	521.	148.8	2.94	463	148.8
67	502.	148.6	2.22	463	148.7
68	395.	143.5	1.24	185	118.0
69	399.	144.3	1.23	188	118.5



B. FLASHING EXPERIMENTS

(Cont'd)

RUN	$P_{in}$ (kPa)	$T_{in}$ ( $^{\circ}$ C)	$G$ (Mg/m <sup>2</sup> s)	$P_{ct}$ (kPa)	$T_{ct}$ ( $^{\circ}$ C)
72	----	----	----	----	----
73	275.	99.4	4.90	56.	87.9
731*	281.	99.4	4.88	52.	88.0
732*	285.	99.4	4.93	52.	87.9
733*	288.	99.4	4.91	53.	88.2
734*	287.	99.4	4.91	54.	88.0
735*	287.	99.4	4.91	55.	88.1
736*	287.	99.4	4.90	54.	88.0
737*	287.	99.4	4.91	54.	87.9
74	285.	99.3	4.90	56.	87.9
75	395.	99.3	6.04	57.	88.5
761	396.	99.3	6.04	60.	88.7
762	393.	99.3	6.05	62.	88.0
763	392.	99.3	6.06	65.	88.0
77	157.	99.3	3.06	65.	88.7
771	157.	99.4	3.03	69.	88.3
78	138.	99.3	2.61	71.	88.0
782	138.	99.3	2.61	71.	88.1
79	124.	99.4	2.27	72.	88.2
791	126.	99.4	2.26	73.	88.1
792	126.	99.4	2.26	83.	88.1
80	585.	148.3	4.36	436.	143.5
803	579.	148.3	4.32	432.	143.5
81	493.	148.3	2.91	432.	144.0
811	493.	148.3	2.91	432.	144.7
814	492.	148.3	2.91	428.	144.1
82	376.	142.3	2.36	174.	111.6
823	377.	142.4	2.32	176.	110.9
83	352.	140.0	2.30	150.	107.9
833	348.	139.5	2.29	145.	107.1

\*Runs 731 through 737 are subsets of Run 73 as are other runs in the hundreds subsets of their decade base, -27-

575 059

from  $9 \times 10^4$  to  $9 \times 10^5$ , based on test section inlet conditions. The raw data for all the single phase calibration experiments are presented in Appendix A. Typical pressure drop results with respect to the inlet and as a function of axial distance are presented in Fig. (5.1) for several flow conditions. In the converging section, the flow acceleration is accompanied by a pressure drop. The deceleration in the diverging section results in an expected pressure recovery. The unrecovered pressure loss at the nozzle exit is representative of the friction losses. Figure (5.2) is a plot of the nondimensionalized pressure drop data obtained from 19 different experiments. The quantities  $\rho$  and  $U_0$  are the density and the velocity at the inlet of the test section. The dots represent the average of the pressure drop, and the bars the standard deviation of all the experiments performed. This maximum deviation is  $< 5$  percent in the converging section, reaches 6 percent at the throat, and reaches a maximum of 10 percent in the diverging section. The single curve corresponds to the pressure distribution due to acceleration only, and was calculated from the geometrical inside diameter measurements. This hydrodynamic calibration provides an effective hydrodynamic area distribution for the test section and will be used for comparison with the flashing data.

## 5.2. Pressure Distributions Under Flashing Conditions

Referring to a p-T diagram such as that in Fig. (5.3), showing the equilibrium vapor pressure  $p_{sat}$  of the liquid, the isothermal expansion of the test liquid in the nozzle may be represented by a vertical line A-B. Here, point A designates the nozzle inlet condition  $(p_{in}, T_{in})$  and point B

SYMBOL	RUN	G(Mg/m <sup>2</sup> s)	P <sub>in</sub> (kPa)	T <sub>in</sub> (C)	P <sub>c.t.</sub> (kPa)
○	10	1.56	711	27	683
□	9	3.13	709	27.1	674
◇	8	4.71	695	26.9	652
△	7	6.30	691	27.3	657
x	6	7.01	682	27.7	647

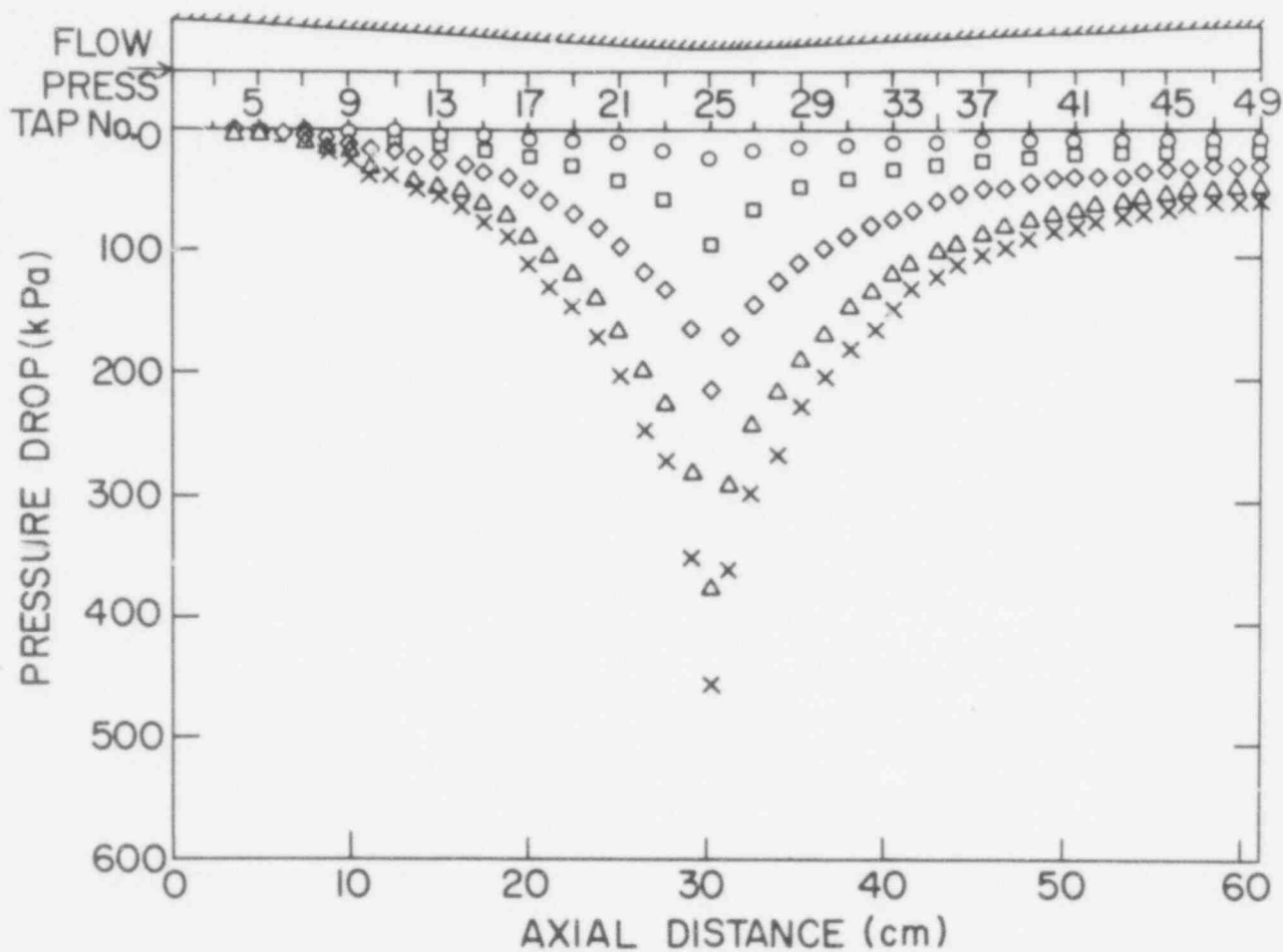


Figure 5.1 Typical Pressure Distributions Along TS-2 for the Single-Phase Flow Hydrodynamic Calibration Runs (BNL Neg. No. 3-1017-79)

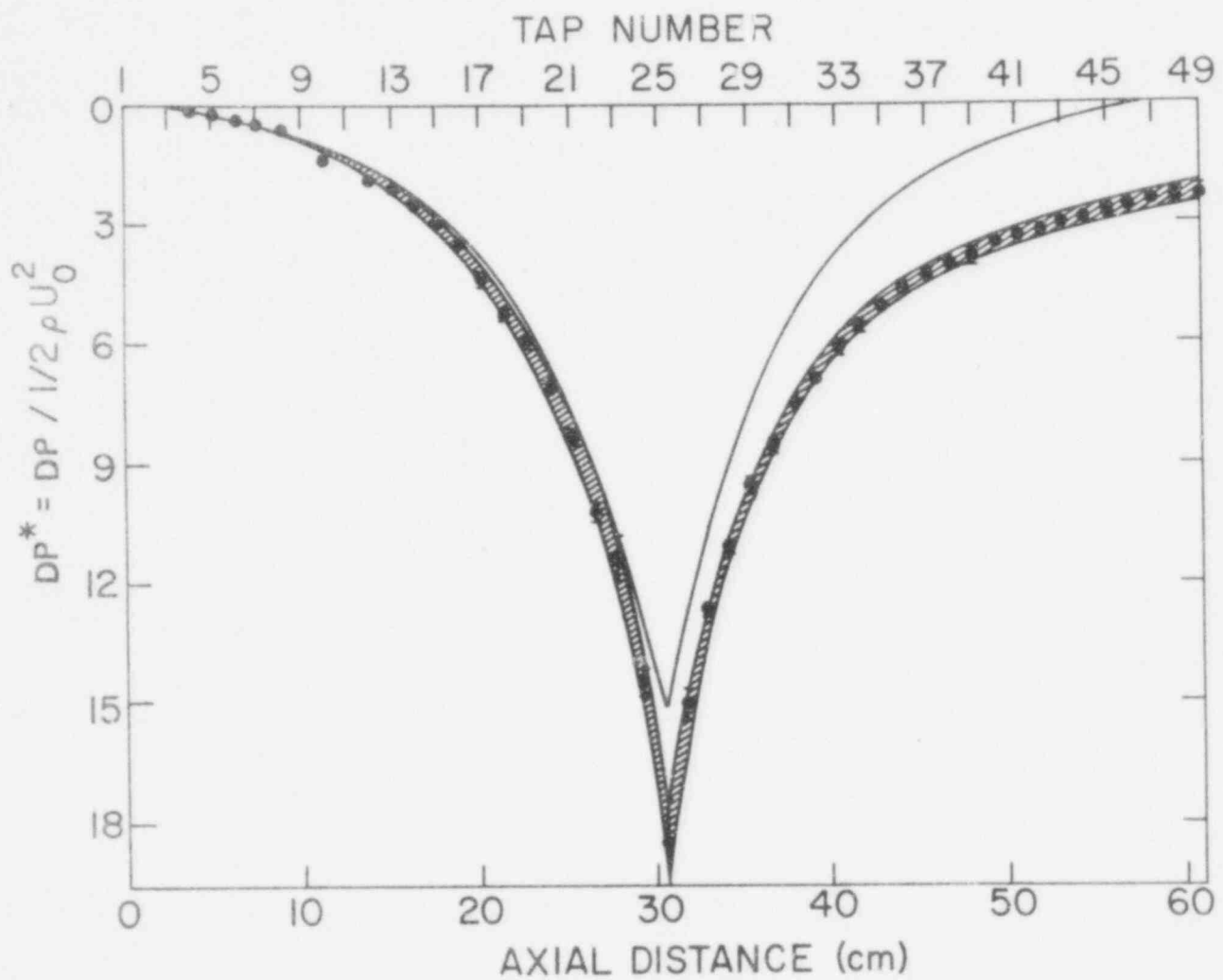


Figure 5.2 Dimensionless Pressure Distribution for TS-2. Data is Averaged for all the Hydrodynamic Calibration Runs Performed (BNL Neg. No. 3-1022-79)

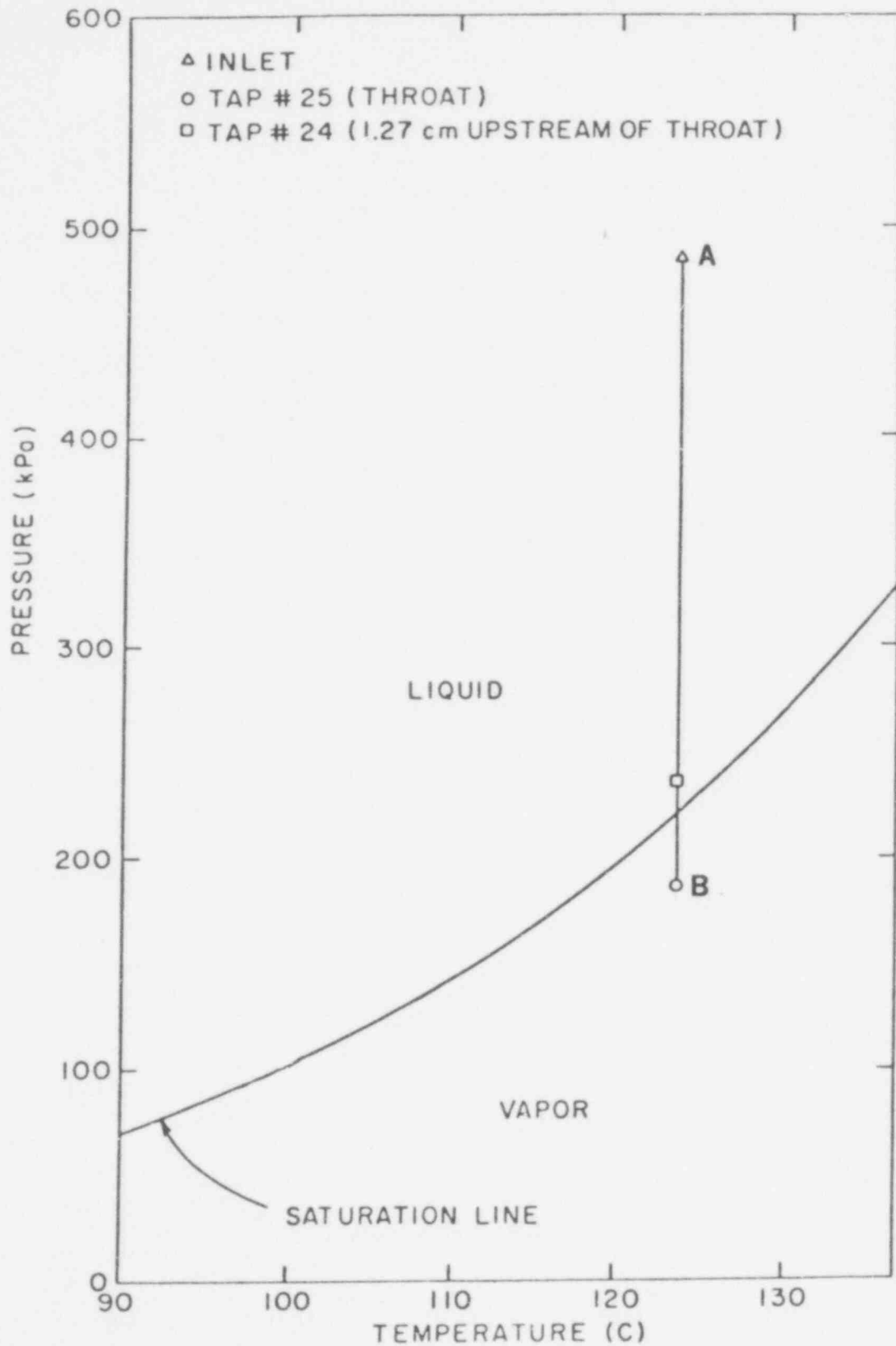


Figure 5.3 Typical Representation of an Isothermal Flashing Experiment in the p-T Diagram (BNL Neg. No. 3-1027-79)

that at the throat. The distance A-B is directly related to the mass flux  $G$  through the nozzle. Thus, for a given inlet condition, the saturation line may be crossed in the expansion if  $G$  is above a certain value.

Figure (5.4) presents typical pressure distributions obtained at inlet temperature of  $100^{\circ}\text{C}$  and four flow rates. At the low mass flux,  $1.81 \text{ Mg/m}^2\text{s}$  (Run 25), very little or almost no flashing was observed at all, and the results are very similar to the single phase calibration data. At the highest mass flux,  $6.01 \text{ Mg/m}^2\text{s}$  (Run 21), the pressure is observed to drop in the converging section up to the throat and level off from there onwards in the diverging section. At intermediate mass fluxes,  $4.90 \text{ Mg/m}^2\text{s}$  (Run 20) and  $5.90 \text{ Mg/m}^2\text{s}$  (Run 28) the results show a constant pressure region downstream of the throat followed by a pressure recovery region in the diverging section of the test section. This sudden pressure increase in the diverging section is caused by a condensation region to accommodate the back pressure imposed on the system. The dimensionless form of the pressure drop data presented in Fig. (5.4) are plotted in Fig. (5.5) vs the axial distance along the test section. The observations about the pressure recovery regions in the diverging section mentioned above are more obvious in this figure. The good agreement of the low mass flux pressure distribution results with the single phase calibration curve was interpreted to mean that no vapor was present in the pressure lines after the flashing experiments.

Similar experiments with flashing flows were also conducted at inlet temperatures of  $124$ ,  $130$ , and  $150^{\circ}\text{C}$  for various flow rates and are tabulated in Appendix B. If one were to plot all these experiments on a  $p$ - $T$  diagram like Fig. (5.3), it would be found that the saturation line was crossed at a

SYMBOL	RUN	G(Mg/m <sup>2</sup> s)	p <sub>in</sub> (kPa)	T <sub>in</sub> (C)	p <sub>c.t.</sub> (kPa)
◇	23	1.81	130	99.4	121
□	28	5.90	566	131.7	316
△	20	4.90	281	98.3	245
○	21	6.01	393	100.6	136

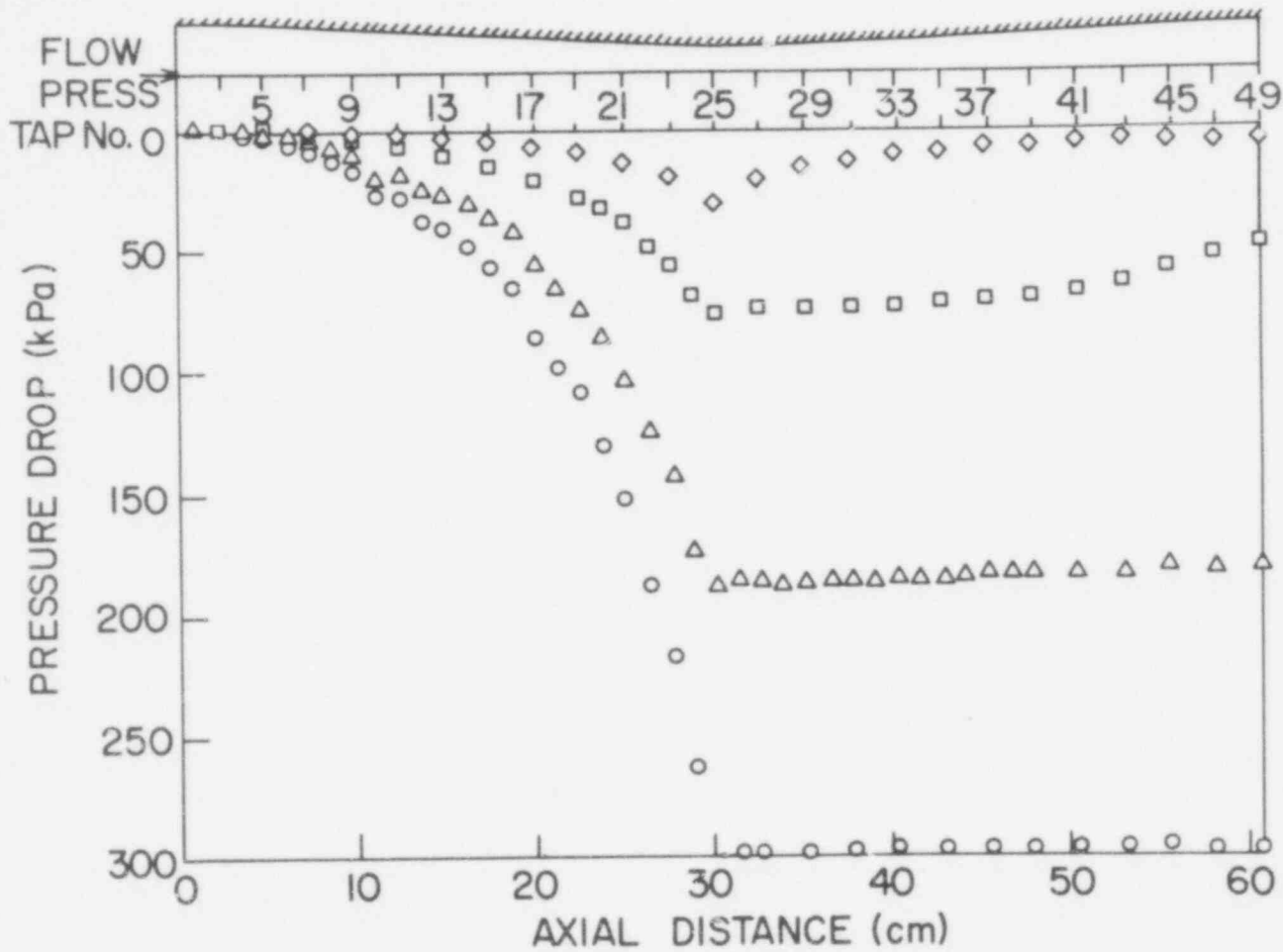


Figure 5.4 Pressure Distributions Under Flashing and Nonflashing Conditions in TS-2 (BNL Neg. No. 3-1019-79)

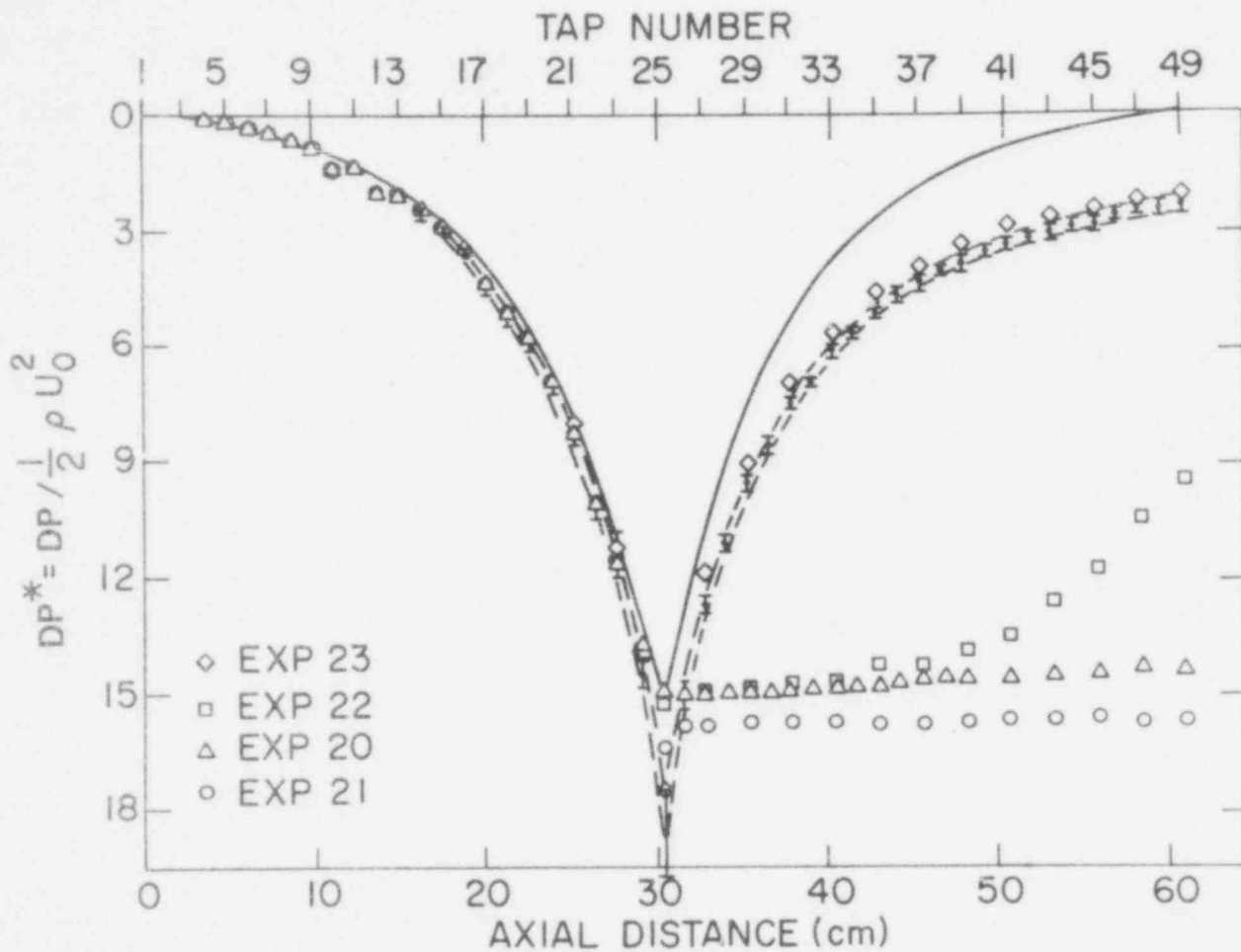


Figure 5.5 Dimensionless Pressure Distributions in TS-2 Under Flashing Conditions as Compared to Single-Phase Hydrodynamic Calibration Data (BNL Neg. No. 3-1021-79)



location upstream and close to the throat in each experiment. Thus we concluded that in most of the experiments reported, flashing occurred at a location upstream but close to the throat. In some later experiments, the flashing front was moved well upstream of the throat.

#### 5.2.1. Reproducibility Studies

To check the repeatability of the data, several runs were performed at nearly identical inlet conditions and flow rates. Figure (5.6) shows the comparison between the pressure distributions obtained in the two experiments for  $p_{in} = 168$  kPa,  $T_{in} = 100^{\circ}\text{C}$ , and mass flux of  $3.03 \times 10^3$  kg/m<sup>2</sup>sec. Experiments were also performed at a higher mass flux  $4.45 \times 10^3$  kg/m<sup>2</sup>sec and  $T_{in} = 123^{\circ}\text{C}$  and  $p_{in} = 390$  kPa. Figure (5.7) depicts the pressure distributions for these latter cases, i.e., Exps. 52 and 53. The results at these mass fluxes are reproducible to within 2 percent.

#### 5.2.2. Operational Effects (Effect of Back Pressure)

In one set of experiments, flashing was initiated with the condensing tank liquid level (defined as the location of the free surface below the top of the tank) equal to zero, i.e., almost a solid loop condition. Decreasing the condensing tank liquid level, i.e., increasing the size of the steam cavity in the condensing tank, changed the downstream (condensing tank) pressure and affected the flashing conditions and pressure distributions although the flow rate and inlet conditions were held constant. Figure (5.8) depicts the pressure distribution results for these experiments, Runs 35, 37, and 43. The pressure distributions in the converging section and mass flux are observed to be independent of the downstream pressure, which imply that the flow is choked. Run 35 depicts the above-mentioned constant

RUN	$G(\text{Mg}/\text{m}^2\text{s})$	$P_{in}(\text{kPa})$	$T_{in}(\text{C})$	$P_{c.t.}(\text{kPa})$
22	3.04	170	100.2	125
40	3.02	168	100.3	112

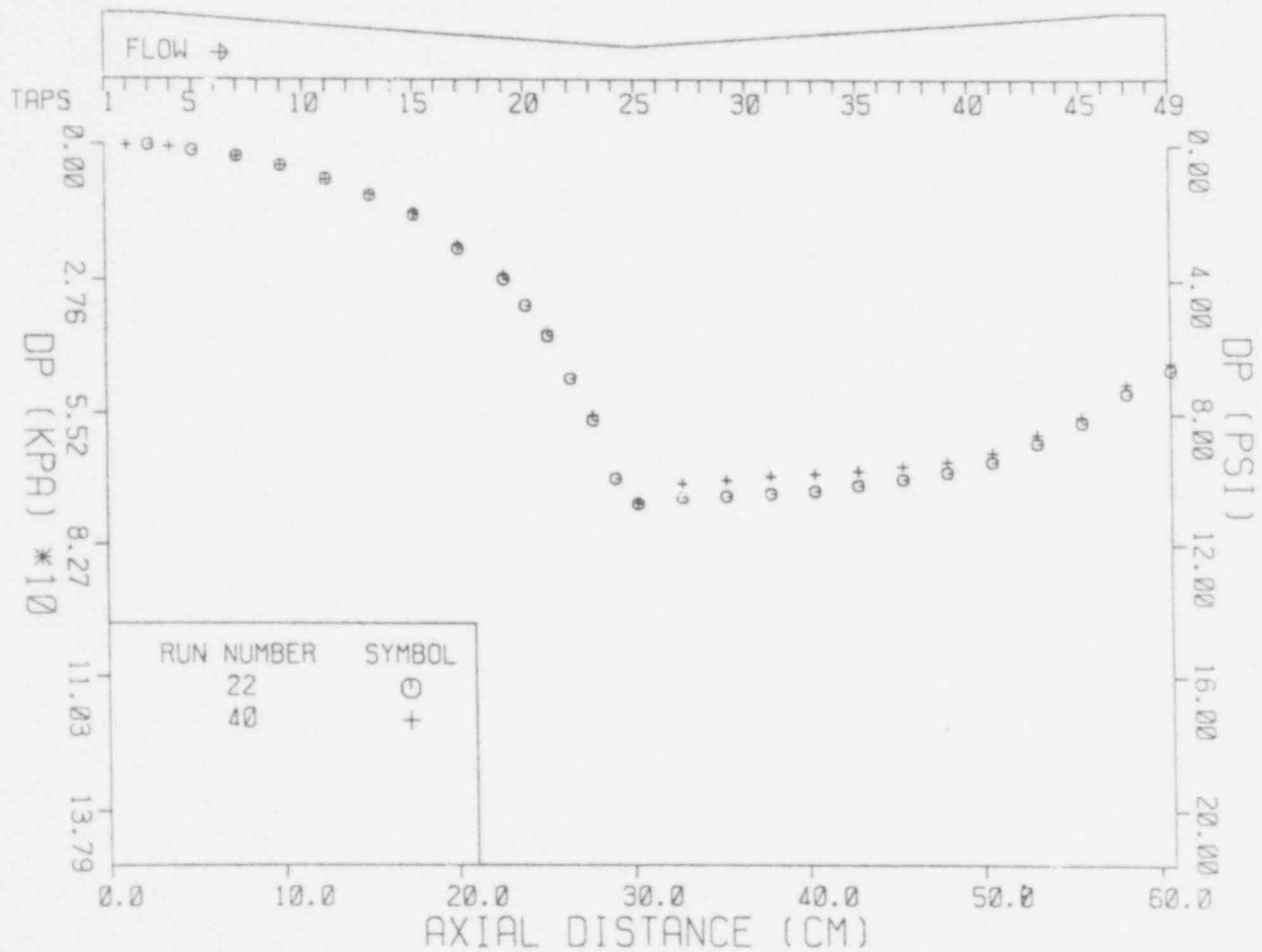


Figure 5.6 Comparison of Pressure Distribution in Two Experiments to Show the Reproducibility of the Results at Low Mass Fluxes,  $G = 3.03 \text{ Mg}/\text{m}^2\text{s}$  (BNL Neg. No. 3-1029-79)

RUN	$G(\text{Mg}/\text{m}^2\text{s})$	$P_{in}(\text{kPa})$	$T_{in}(\text{C})$	$P_{c.t.}(\text{kPa})$
52	4.48	381	123.5	254
53	4.45	395	123.6	249

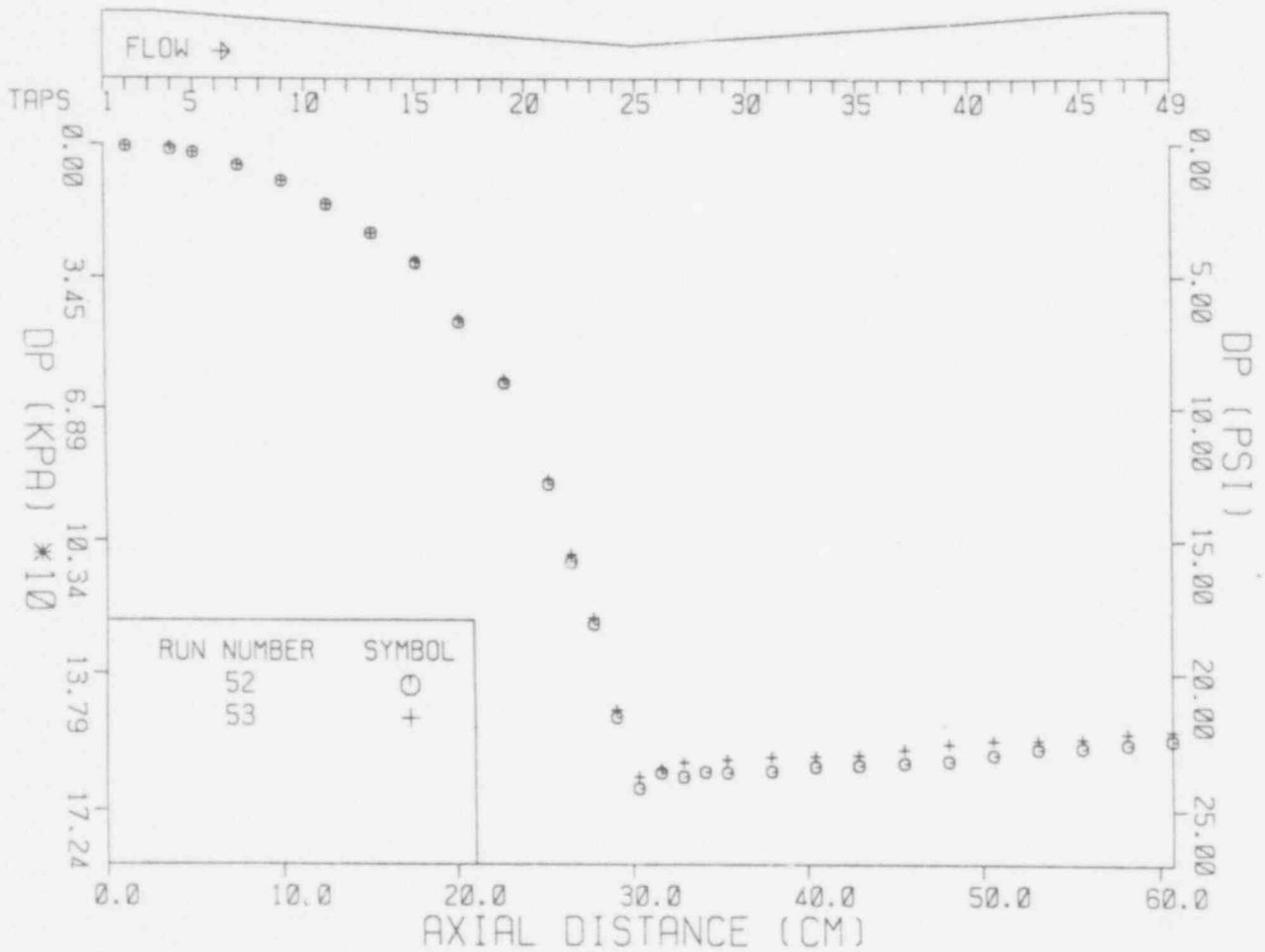


Figure 5.7 Comparison of Pressure Distributions in Two Experiments to Show Reproducibility of the Results at High Mass Flux,  $G = 4.45 \text{ Mg}/\text{m}^2\text{s}$  (BNL Neg. No. 3-1028-79)

RUN	G(Mg/m <sup>2</sup> s)	p <sub>in</sub> (kPa)	T <sub>in</sub> (C)	p <sub>c.t.</sub> (kPa)
35	4.96	287	99.4	250
37	4.94	296	100.3	170
43	4.97	287	100.2	120

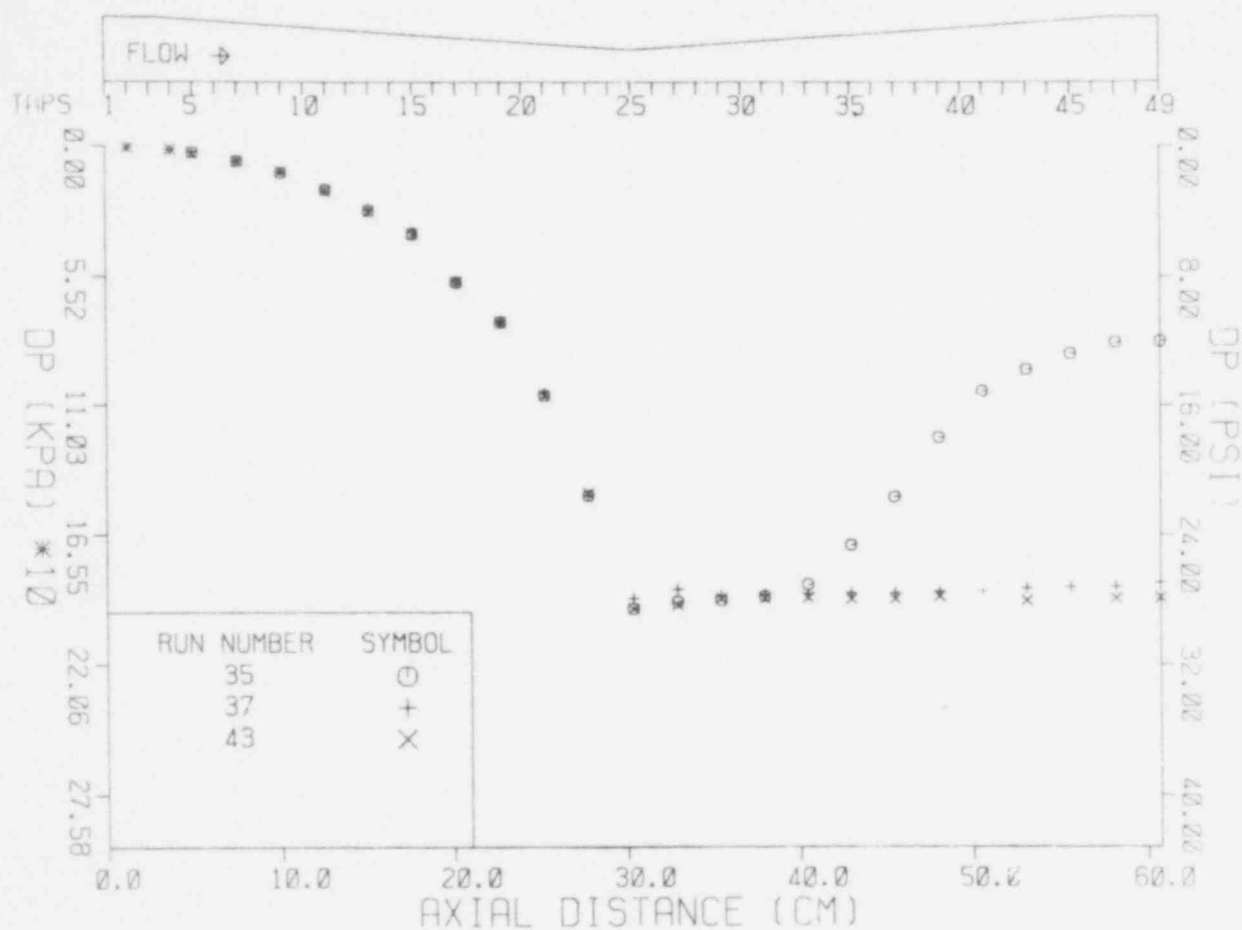


Figure 5.8 Pressure Distributions Showing the Effect of Condensing Tank Back Pressure for Identical Nozzle Inlet Conditions (BNL Neg. No. 3-1031-79)

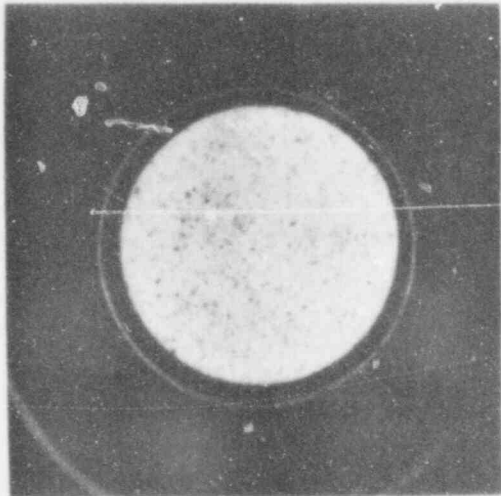
pressure region downstream of the throat followed by a sudden pressure rise, which seems to correspond to a condensation region as previously described. Runs 37 and 43 are almost identical although the condensing tank pressure is lower in Run 43.

The photographic observations performed during these experiments are presented in Fig. (5.9). For Run 35, the bubble sizes are minute, and their number density is very large. Decreasing the back pressure increases the vapor generated in Runs 37 and 43. During Run 43, the windows were covered with a water film, and the interior of the tube was invisible. This drastic difference in observed appearance between Runs 37 and 43, does not noticeably affect the pressure distributions presented in Fig. 5.8.

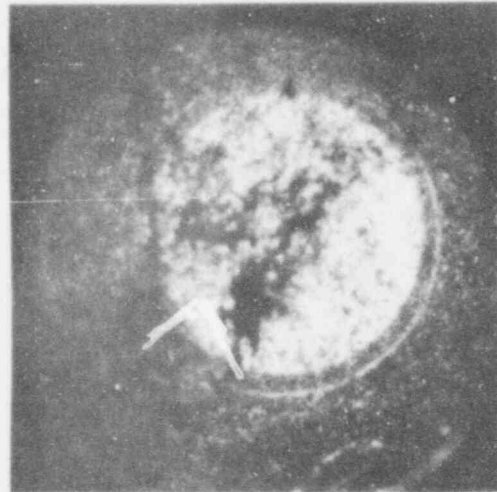
### 5.2.3. Parametric Effects

The effects of the flow parameters, i.e., inlet pressure,  $p_{in}$ , inlet temperature,  $T_{in}$ , and mass flux,  $G$ , in the flashing regimes and pressure distributions were also investigated and will be presented below. Figure (5.10) presents the results when  $p_{in}$  and  $T_{in}$  were kept constant and the mass flux was varied close to conditions of flashing onset in the nozzle. This is equivalent to lengthening or shortening the line A-B in Fig. (5.3), moving the point B near the  $p_{sat}$  curve. The pressure distribution in the converging part follows very closely the single phase calibration. Downstream of the throat the vapor generation manifests itself as a deviation in the pressure distribution. This region is followed by a pressure increase caused by the sudden collapse of the bubbles and followed by a pressure recovery zone typical of single phase flows in divergent pipes. Figure (5.11) depicts the photographic observations for these two cases. Although

# POOR ORIGINAL



A. RUN NO. 35



B. RUN NO. 37



C. RUN NO. 43

SCALE 1:1

Figure 5.9 Photographic Observations for the Experimental Conditions Presented in Fig. (5.8). In these and all the following photographs, the diameter of both the front and rear windows is 50 mm. (BNL Neg. No. 1-919-79).

RUN	G(Mg/m <sup>2</sup> s)	p <sub>in</sub> (kPa)	T <sub>in</sub> (C)	p <sub>c.t.</sub> (kPa)
49	2.27	146	99.9	99
50	2.04	142	99.8	101

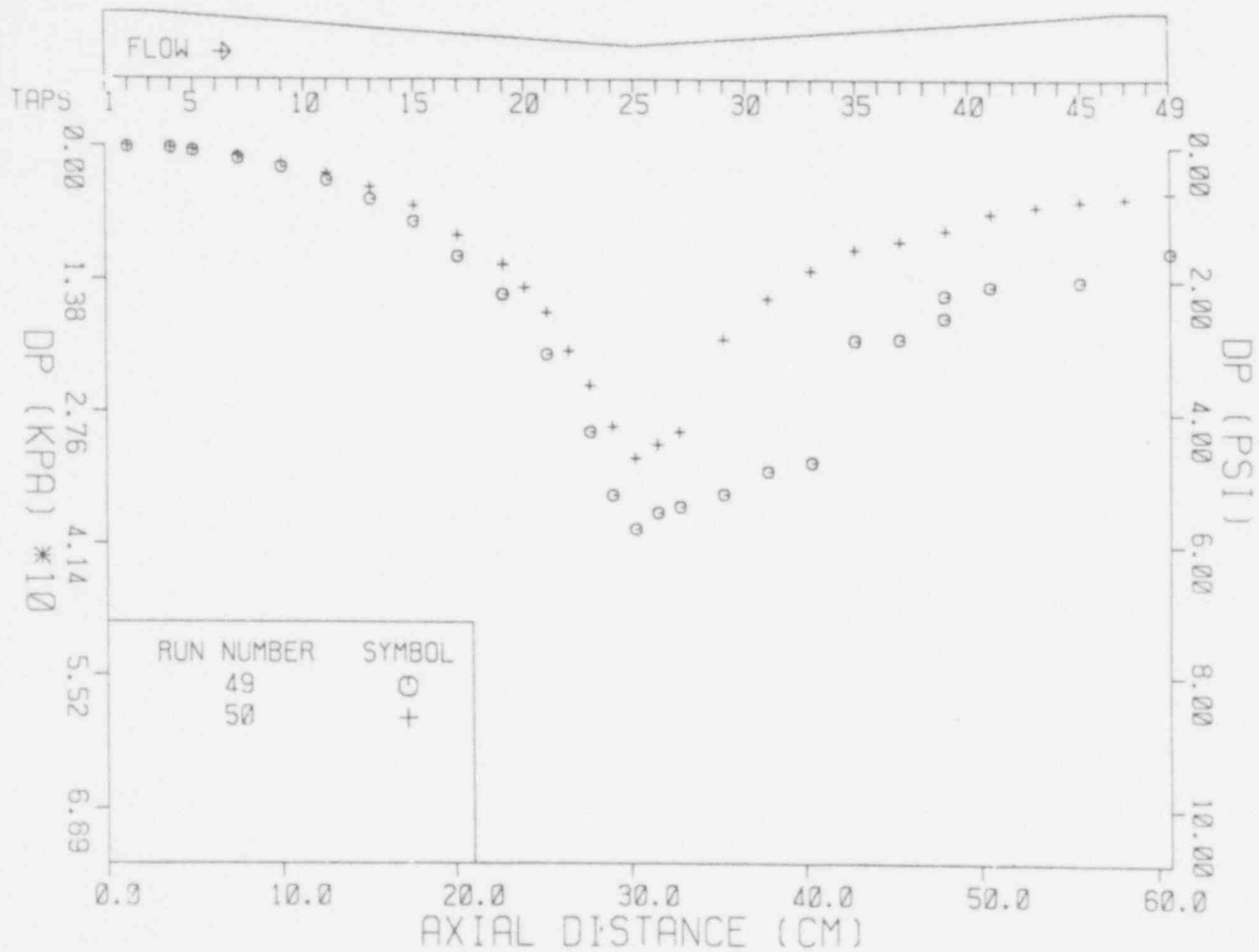
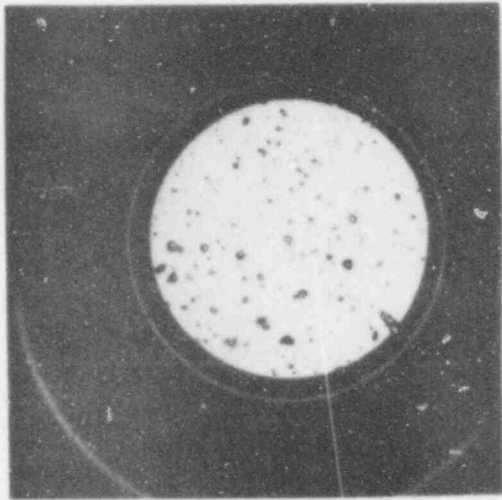


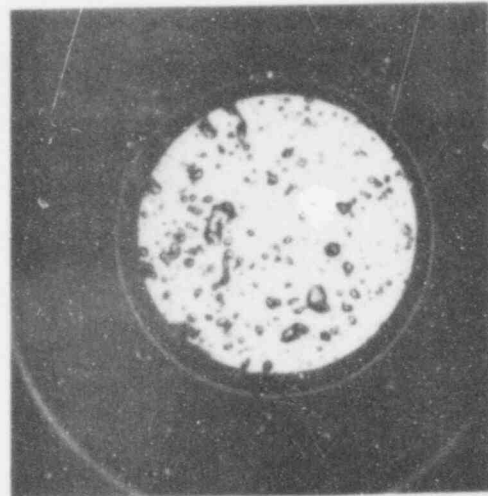
Figure 5.10 Effect of Mass Flux on Pressure Distributions for Identical Nozzle Inlet Conditions Which are Close to the Onset of Flashing in the Test Section (BNL Neg. No. 3-1032-79).

# POOR ORIGINAL

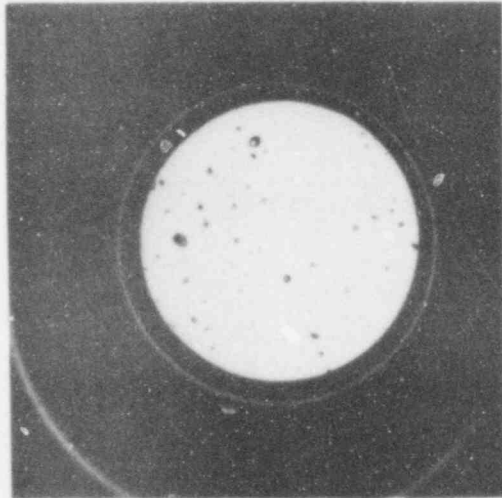
SCALE 1:1



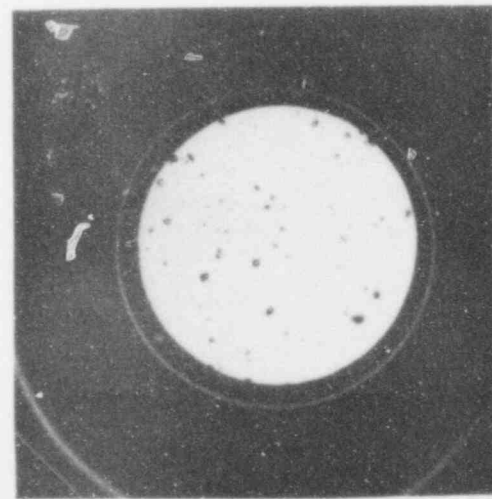
RUN NO. 49



RUN NO. 49



RUN NO. 50



RUN NO. 50

Figure 5.11 Photographic Observations for the Experimental Conditions Presented in Fig. (5.10) (BNL Neg. No. 1-922-79).



the appearance of the bubbles was found to be intermittent, this fact was not apparent in the pressure measurements due to the time response of our pressure manifolds and to our long averaging times. In Fig. (5.12), we present the typical effect of a more substantial change in mass flux for an inlet temperature of  $123^{\circ}\text{C}$  and an inlet pressure of 260 kPa. At a mass flux of  $2.04 \text{ Mg/m}^2\text{s}$  (Run 57), one observes the onset of flashing, which intensified to violent flashing at a mass flux of  $2.98 \text{ Mg/m}^2\text{s}$  (Run 61). The corresponding photographic observations are presented in Fig. (5.13).

The effect of changing the inlet temperature from 100 to  $150^{\circ}\text{C}$  was also investigated while maintaining a fixed initial overpressure,  $p_{\text{in}} - p_{\text{sat}}(T_{\text{in}})$ . This corresponds to moving the point A parallel to the saturation curve  $p_{\text{sat}}$  in Fig. (5.3) and keeping the mass flux unchanged. For constant values of the pressure difference between the inlet pressure and the saturation pressure at the inlet temperature, i.e.,  $p_{\text{in}} - p_{\text{sat}}(T_{\text{in}})$ , the effect of inlet temperature on the pressure distributions was not very pronounced for the various flashing experiments. This behavior was to be expected, since the driving potential, i.e.,  $(p - p_{\text{sat}})$  was not changed in these runs. Figure (5.14) represents these results for Exp. 67 ( $T_{\text{in}} = 149.2^{\circ}\text{C}$ ,  $p_{\text{in}} = 503.3 \text{ kPa}$ ) Exp. 56 ( $T_{\text{in}} = 123.5^{\circ}\text{C}$ ,  $p_{\text{in}} = 136.5 \text{ kPa}$ ) and Exp. 39, while the mass flux is  $2.20 \times 10^3 \text{ kg/m}^2\text{sec}$  for the experimental conditions close to the onset of flashing. The photographic observations for Exps. 39 and 56 are presented in Fig. (5.15). One observes that the effect of inlet temperature is small as long as the inlet pressure is adjusted for constant subcooling at the inlet. The same observation will be valid for the following results. Figures (5.16), (5.17), and (5.18) show similar results for progressively higher mass fluxes, and Fig. (5.19) show

RUN	$G(\text{Mg}/\text{m}^2\text{s})$	$P_{in}(\text{kPa})$	$T_{in}(\text{C})$	$P_{c.t.}(\text{kPa})$
57	2.04	263	124.7	256
58	2.98	254	123.3	174
61	2.98	259	123.8	162

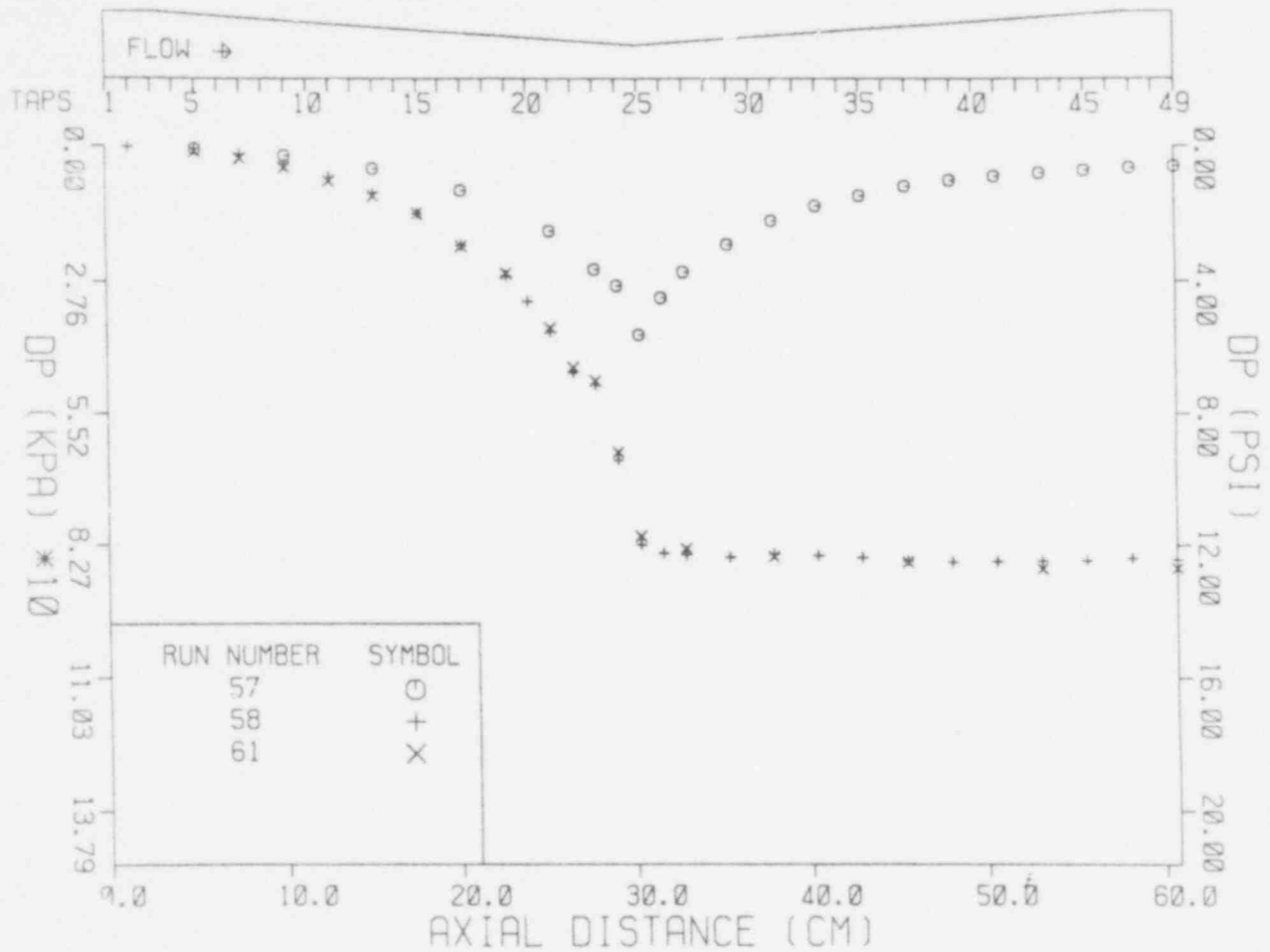
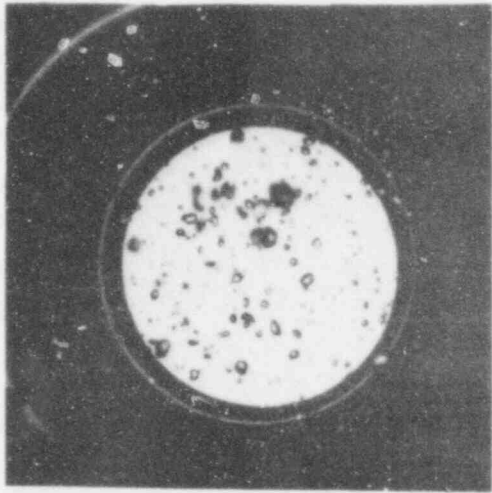
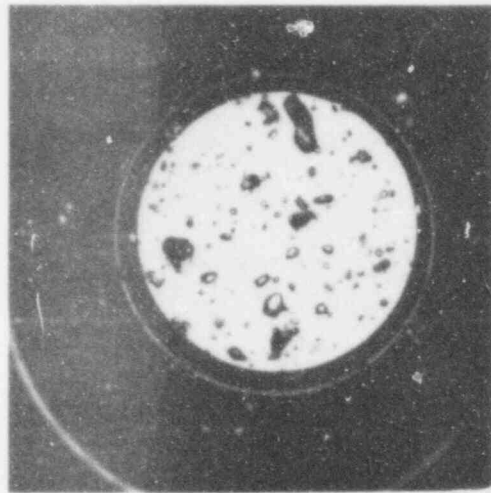


Figure 5.12 Effect of Mass Flux on the Pressure Distributions in the Test Section (BNL Neg. No. 3-1033-79)

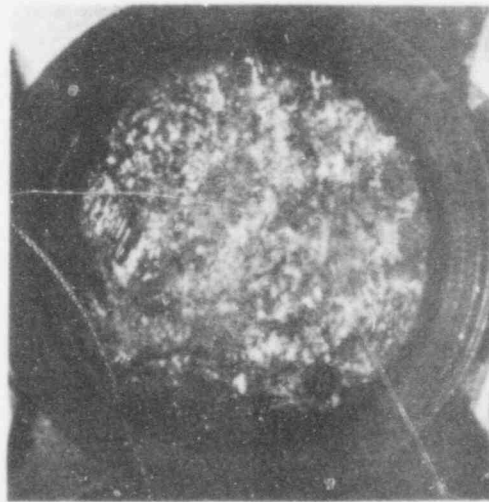
# POOR ORIGINAL



RUN NO. 57



RUN NO. 57



RUN NO. 61

SCALE 1:1

Figure 5.13 Photographic Observations for the Experimental Conditions Presented in Fig. (5.12) (BNL Neg. No. 1-918-79).

RUN	G(Mg/m <sup>2</sup> s)	p <sub>in</sub> (kPa)	T <sub>in</sub> (C)	p <sub>c.t.</sub> (kPa)
67	2.22	502	148.6	463
56	2.20	261	123.2	252
39	2.25	136	100.5	112

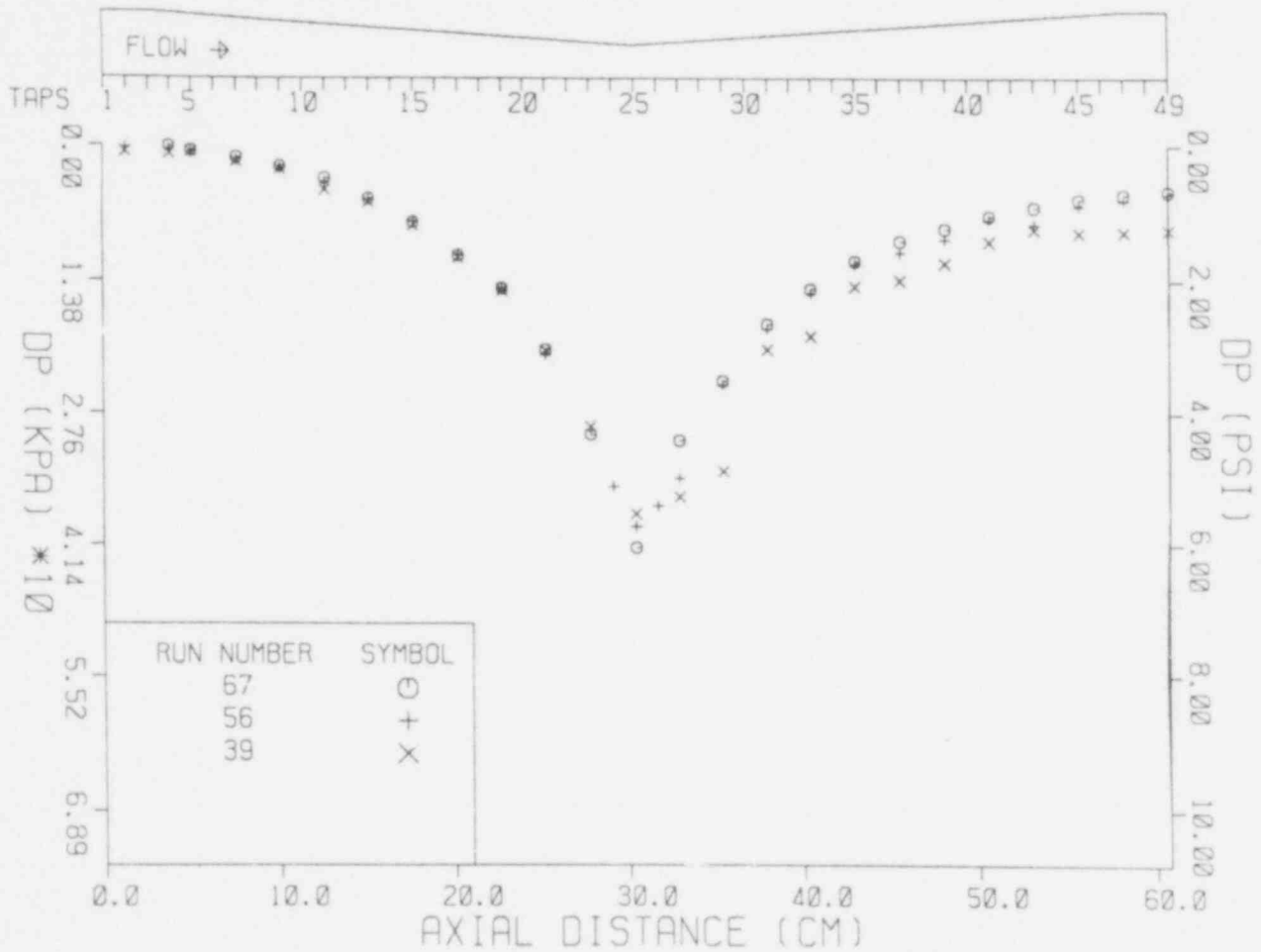
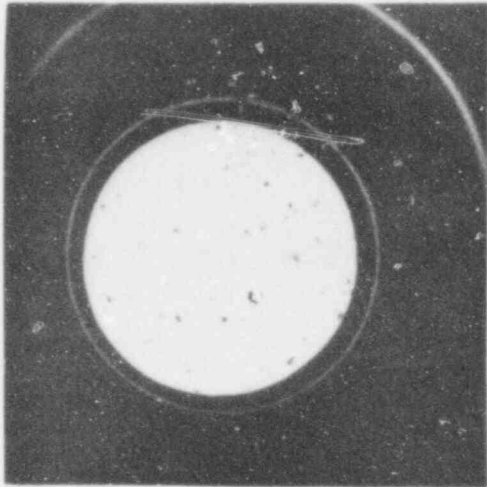


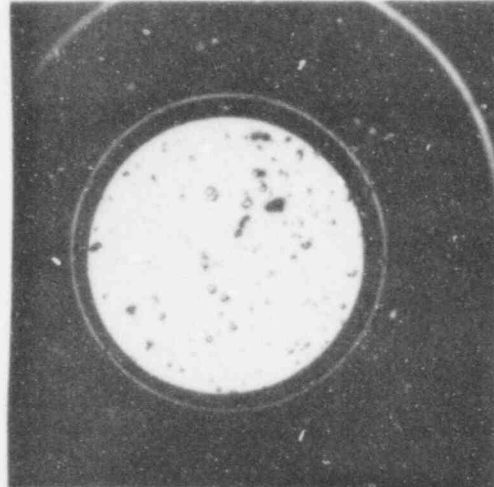
Figure 5.14 Effect of Nozzle Inlet Temperature at Constant ( $p_{in} - p_{sat}(T_{in})$ ) on the Pressure Distribution in the Test Section (BNL Neg. No. 3-1030-79).

# POOR ORIGINAL

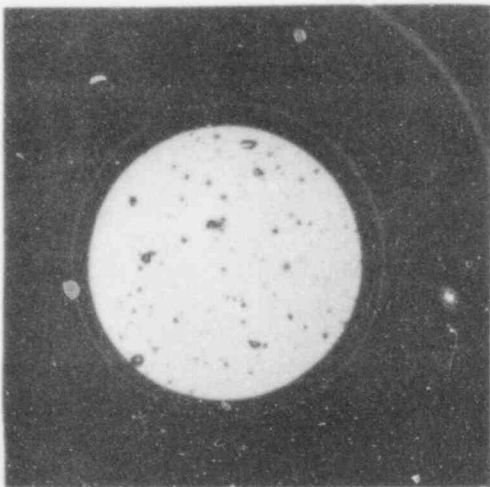
SCALE 1:1



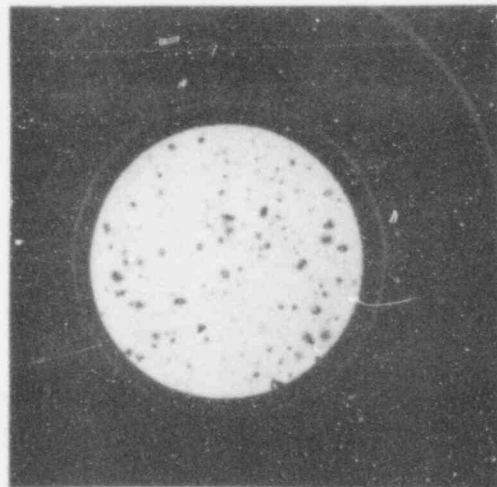
RUN NO. 56



RUN NO. 56



RUN NO. 39



RUN NO. 39

Figure 5.15 Photographic Observations for Experimental Conditions Presented in Fig. (5.14) (BNL Neg. No. 1-921-79).

RUN	G(Mg/m <sup>2</sup> s)	p <sub>in</sub> (kPa)	T <sub>in</sub> (C)	p <sub>c.t.</sub> (kPa)
66	2.94	521	148.8	463
55	2.99	293	123.6	251
27	2.95	326	130.0	299

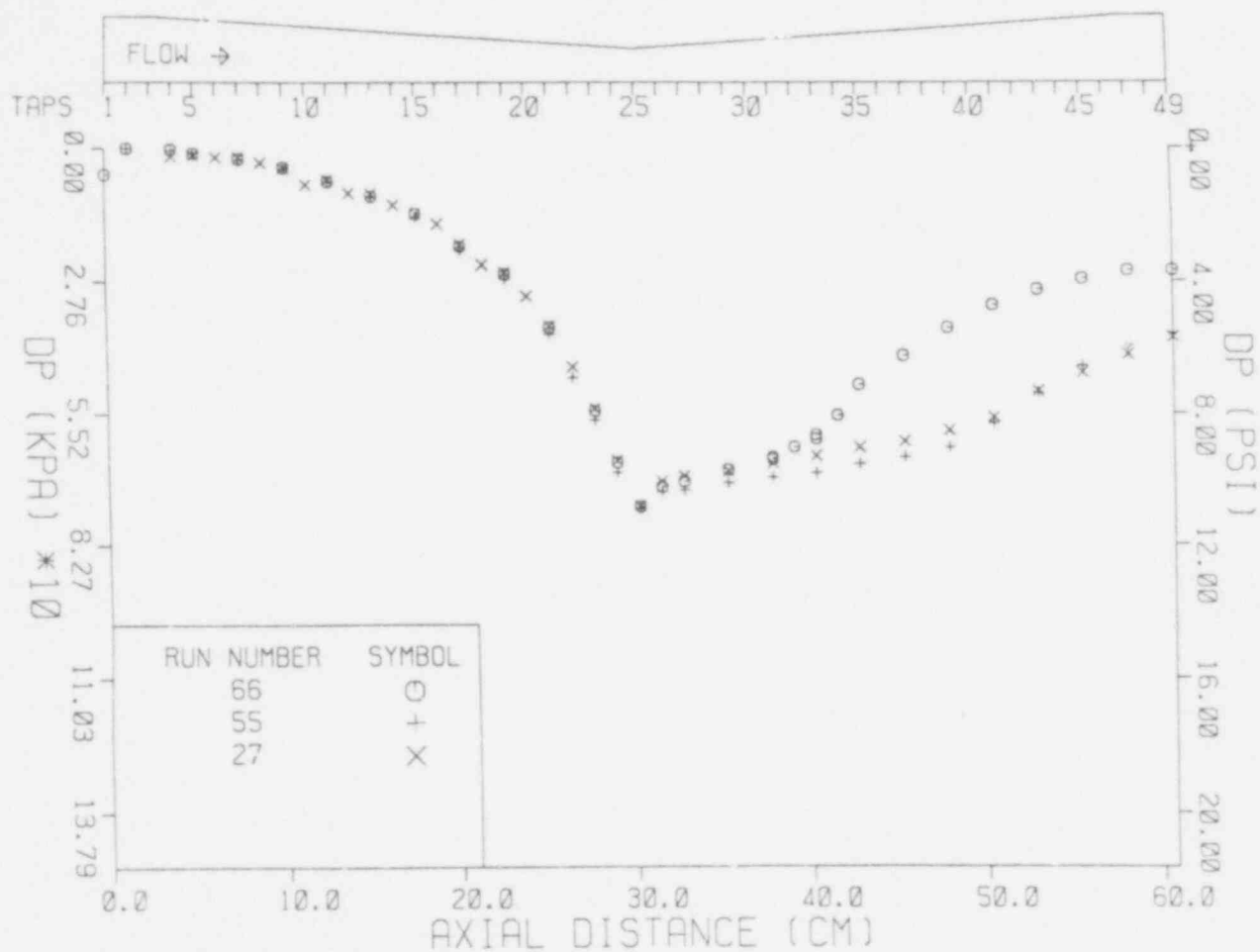


Figure 5.16 Effect of Nozzle Inlet Temperature at Constant (p<sub>in</sub> - p<sub>sat</sub>(T<sub>in</sub>)) on the Pressure Distribution in the Nozzle (BNL Neg. No. 3-1037-79).

RUN	G(Mg/m <sup>2</sup> s)	p <sub>in</sub> (kPa)	T <sub>in</sub> (C)	p <sub>c.t.</sub> (kPa)
22	3.04	170	100.2	125
24	3.05	160	98	122

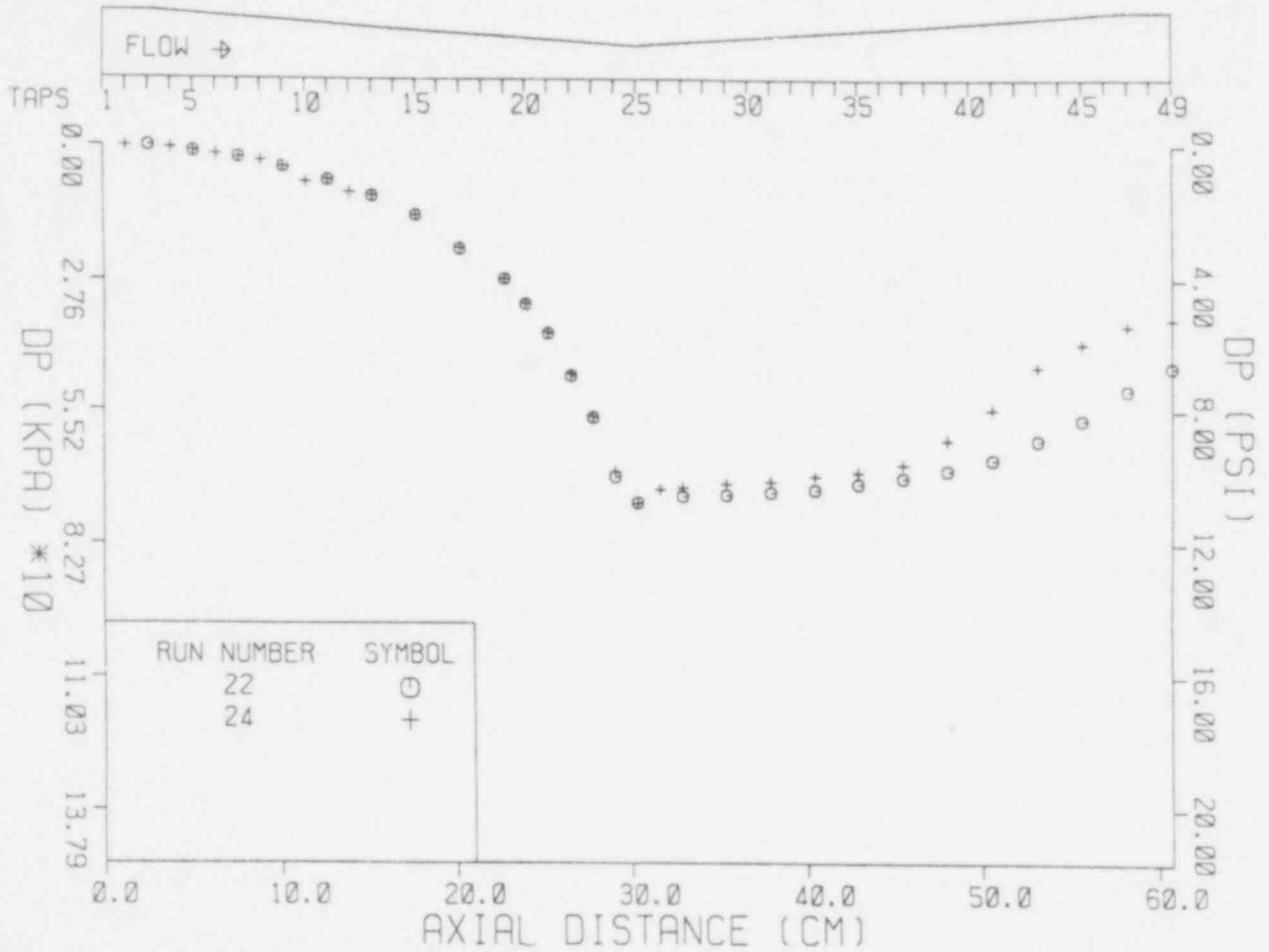


Figure 5.17 Effect of Nozzle Inlet Temperature at Constant ( $p_{in} - p_{sat}(T_{in})$ ) on the Pressure Distribution in the Nozzle (BNL Neg. No. 3-1035-79).

RUN	G(Mg/m <sup>2</sup> s)	p <sub>in</sub> (kPa)	T <sub>in</sub> (C)	p <sub>c.t.</sub> (kPa)
44	4.50	271	99.9	101
52	4.48	381	123.5	254
64	4.40	609	148.8	463

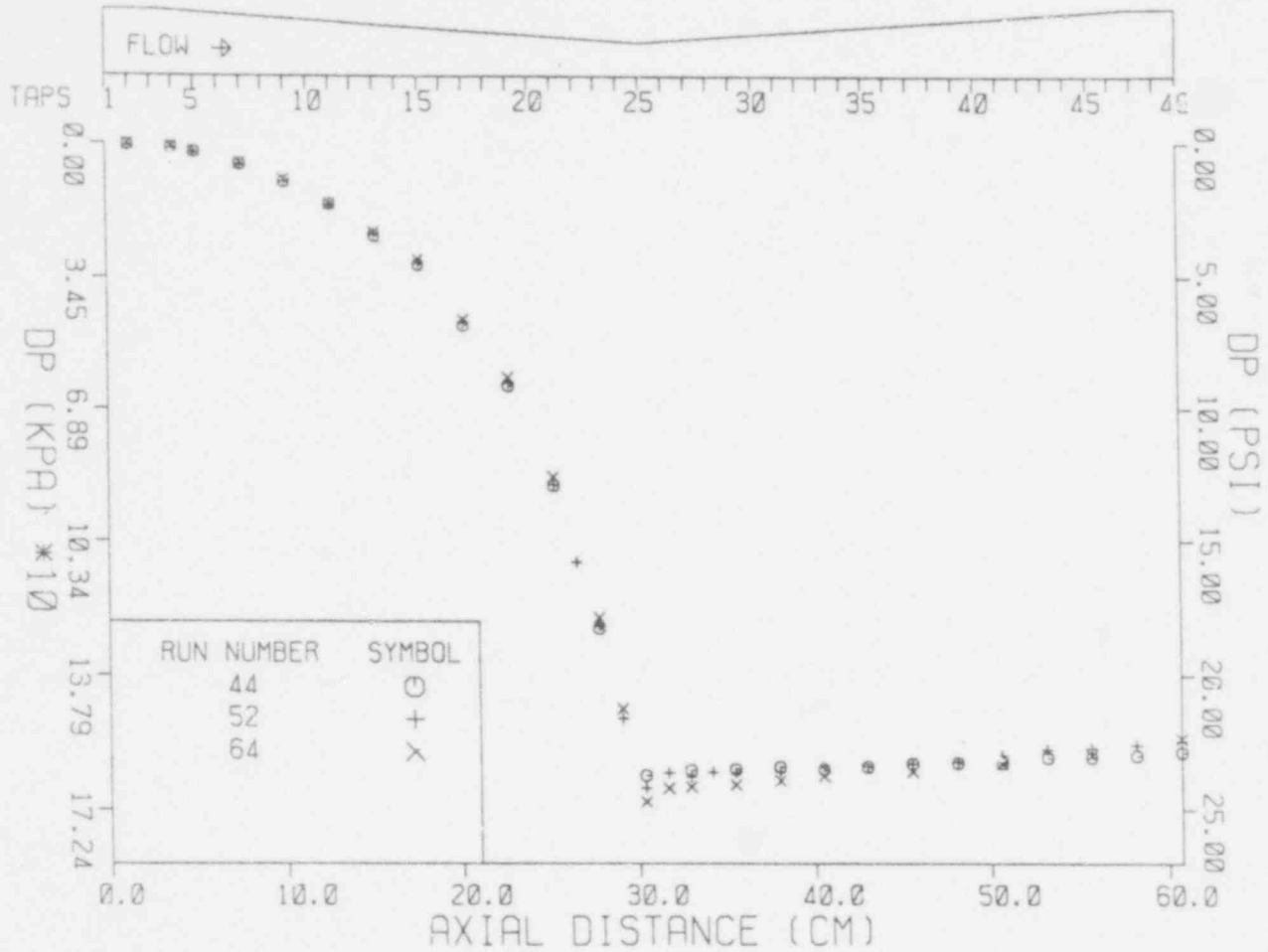
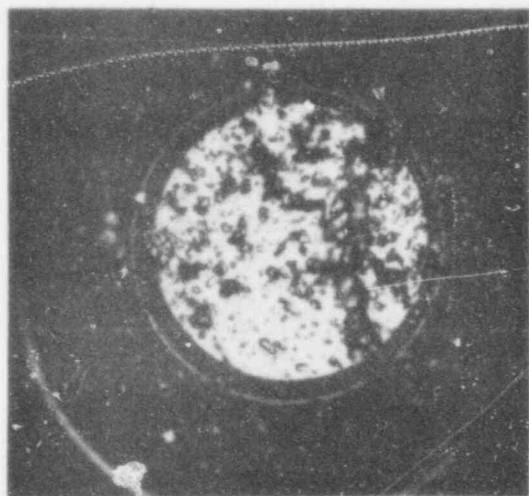


Figure 5.18 Effect of Nozzle Inlet Temperature at Constant ( $p_{in} - p_{sat}(T_{in})$ ) on the Pressure Distribution in the Nozzle (BNL Neg. No. 3-1034-79).

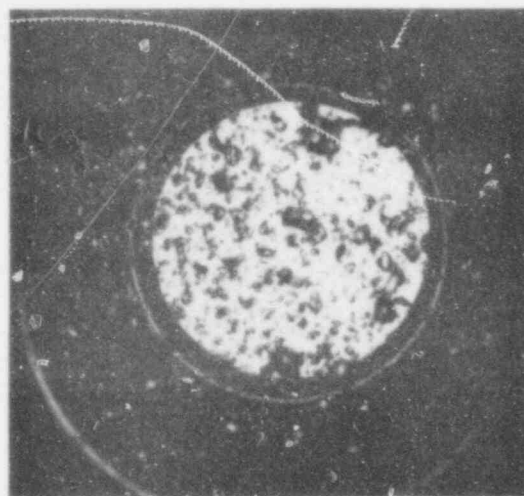


# POOR ORIGINAL

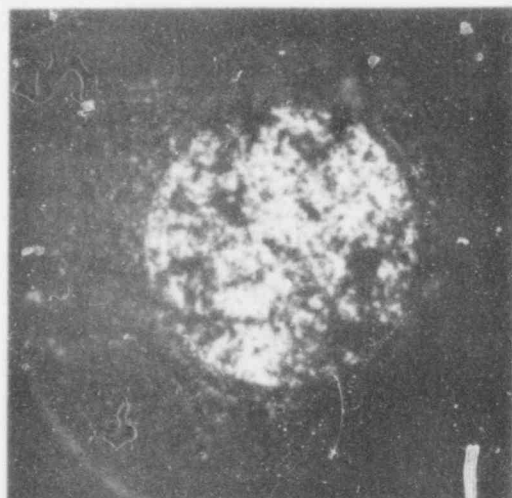
SCALE 1:1



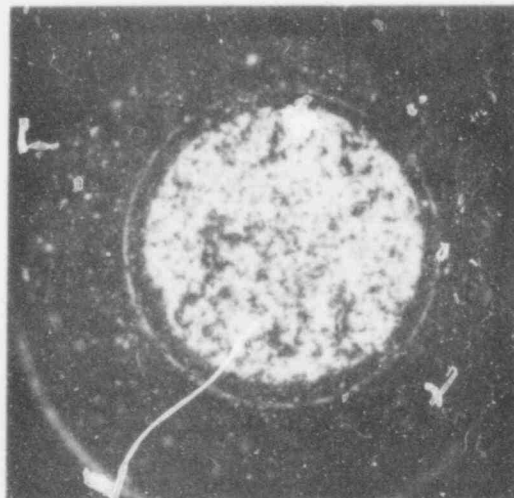
RUN NO. 55



RUN NO. 55



RUN NO. 52



RUN NO. 52

Figure 5.19 Photographic Observations for Experimental Conditions Presented in Fig. (5.16) and (5.18) (BNL Neg. No. 1-920-79).

photographic observations for Exp. 55 and 52.

Finally, the influence of variation of  $p_{in}$ , i.e., moving the point A in Fig. (5.3) up and down without changing anything else, was studied. A slight variation of the inlet pressure was found to affect the pressure distributions and flashing regimes for identical inlet temperatures and mass fluxes. This dependence and sensitivity is more pronounced at low mass fluxes, Fig. (5.20) (Runs 55 and 58 with an inlet temperature of  $123.5^{\circ}\text{C}$  and mass flux of  $2.98 \text{ Mg/m}^2\text{s}$ ). A variation of the inlet pressure from 293 kPa (Run 55) to 254 kPa (Run 58) shows a marked variation in the pressure distributions in the diverging section of the nozzle.\* This strong dependence observed for the low mass fluxes does not repeat itself at the higher mass fluxes, 3.04 and  $4.96 \text{ Mg/m}^2\text{sec}$ , as presented in Figs. (5.21) and (5.22) for an inlet temperature of  $100^{\circ}\text{C}$ .

#### 5.2.4 Flashing Upstream of the Throat

In all the experiments presented above, flashing occurred in the vicinity of the throat. By controlling the flow conditions, we were able to approach saturation conditions at the inlet of the test section. The pressure distribution recorded under this condition is presented in Fig. (5.23). The continuous pressure decrease in the converging, as well as the diverging sections of the nozzle, is reminiscent of the supercritical flows in supersonic nozzles in classical gasdynamics. The onset of flashing, which is accompanied with a strong deviation in the pressure distribution as compared to the single phase calibration, is depicted in Fig.

---

\* Note that in these two experiments, the condensing tank pressure also varied from 174 kPa (Exp. 58) to 251 kPa (Exp. 55).

RUN	G (Mg/m <sup>2</sup> s)	P <sub>in</sub> (kPa)	T <sub>in</sub> (C)	P <sub>c.t.</sub> (kPa)
55	2.99	293	123.6	251
58	2.98	254	123.3	174

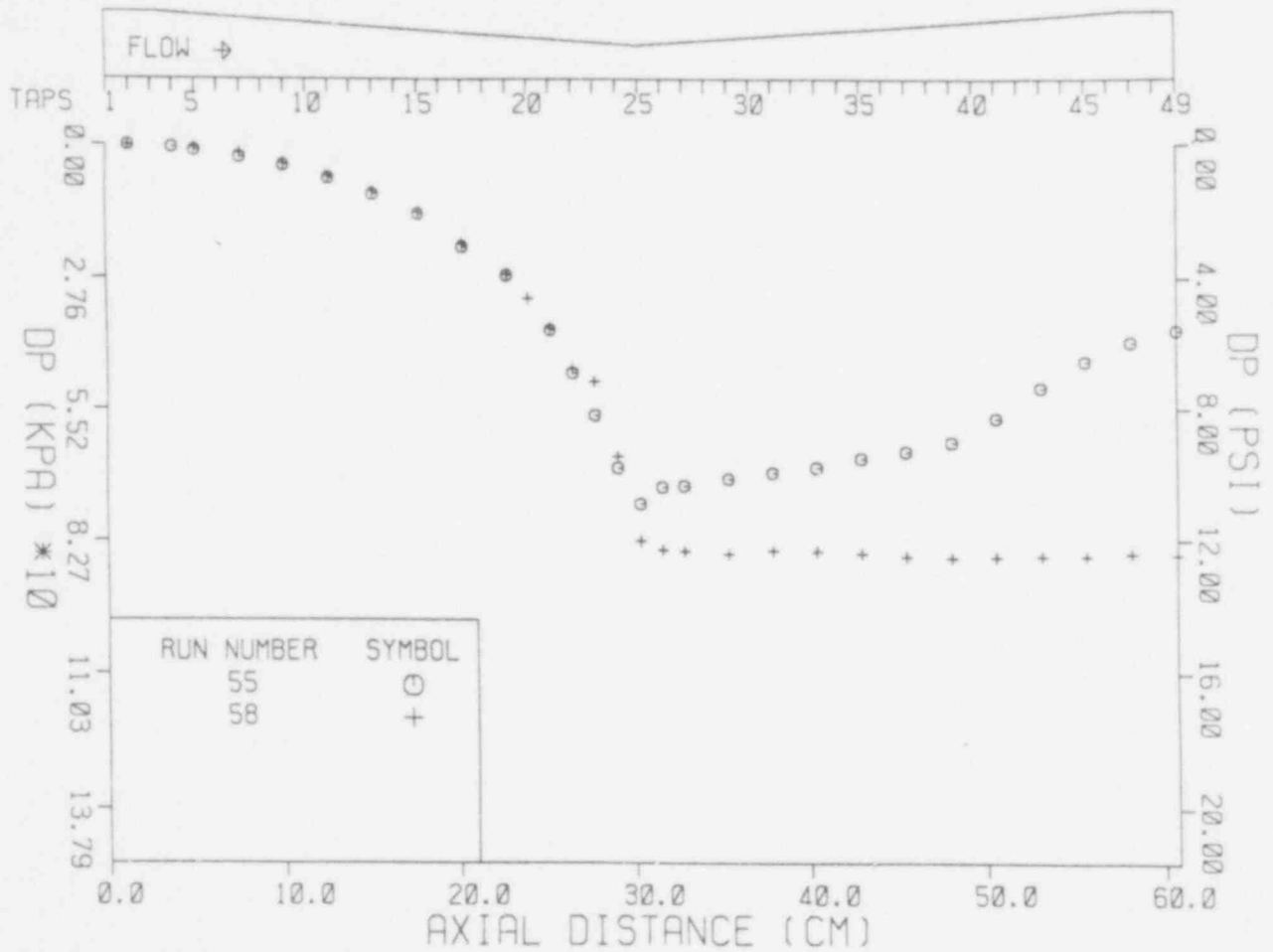


Figure 5.20 Effect of Nozzle Inlet Pressure on the Pressure Distributions in the Test Section (BNL Neg. No. 3-1036-79)

RUN	$G(\text{Mg}/\text{m}^2\text{s})$	$P_{in}(\text{kPa})$	$T_{in}(\text{C})$	$P_{c.t.}(\text{kPa})$
22	3.04	170	100.2	125
48	3.04	183	99.9	100

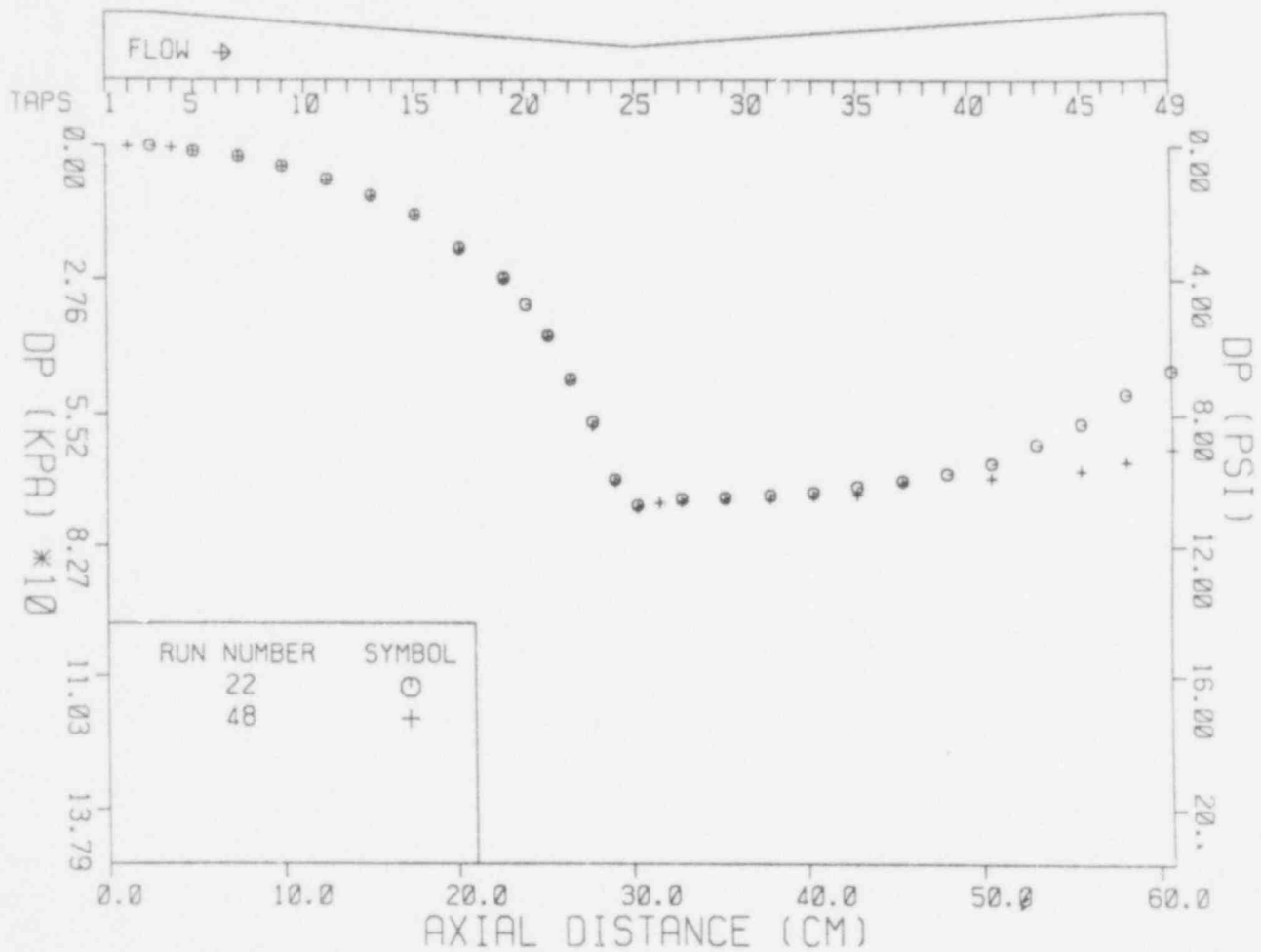


Figure 5.21 Effect of Nozzle Inlet Pressure on the Pressure Distributions in the Test Section (BNL Neg. No. 3-1023-79)

575 086

RUN	$G(\text{Mg}/\text{m}^2\text{s})$	$P_{in}(\text{kPa})$	$T_{in}(\text{C})$	$P_{c.t.}(\text{kPa})$
45	4.97	308	99.8	99
37	4.94	296	100.3	170
43	4.97	287	100.2	121

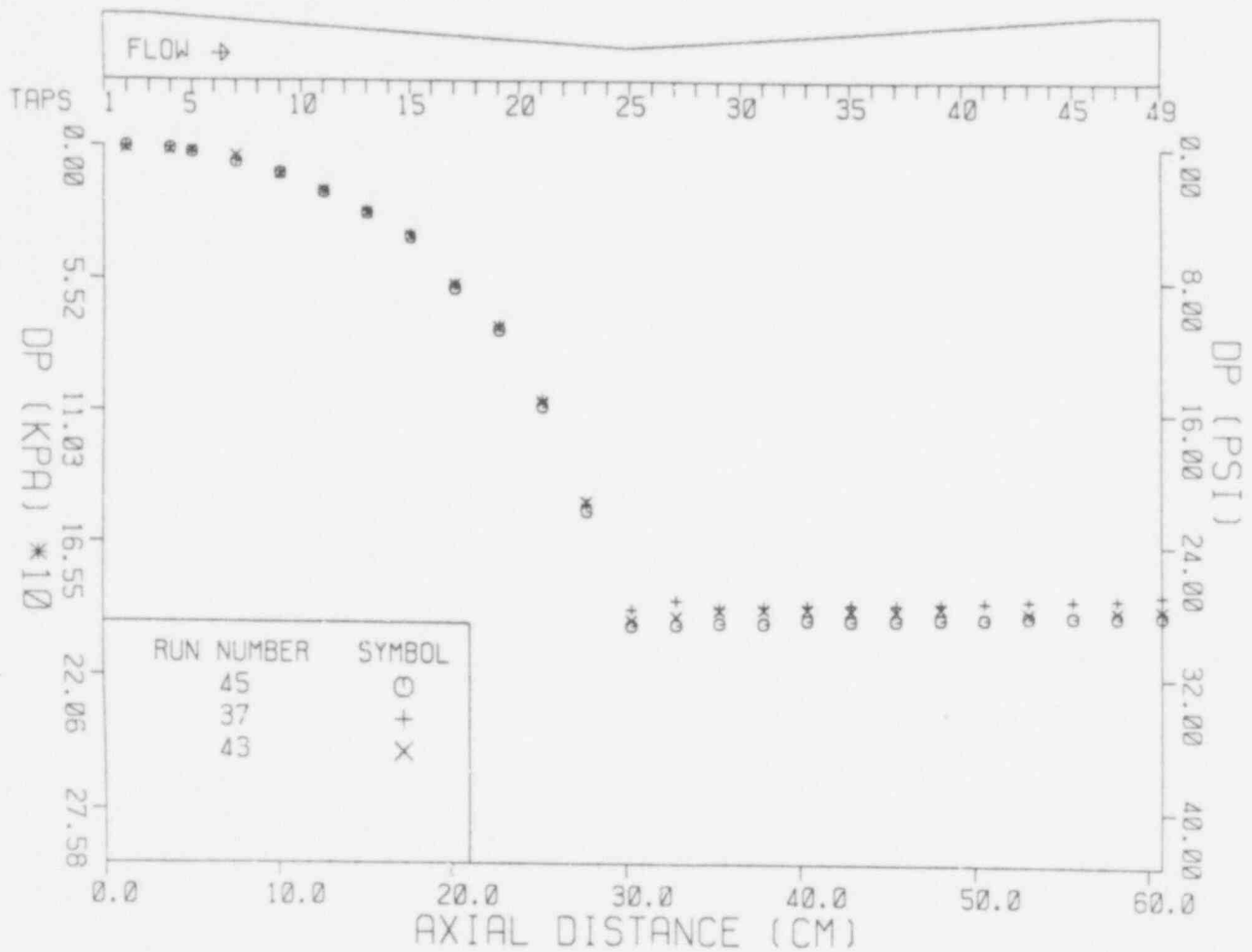


Figure 5.22 Effect of Nozzle Inlet Pressure on the Pressure Distributions in the Test Section (BNL Neg. No. 3-1025-79)

RUN	G(Mg/m <sup>2</sup> s)	P <sub>in</sub> (kPa)	T <sub>in</sub> (C)	P <sub>c.t.</sub> (kPa)
69	1.23	399	144.3	188

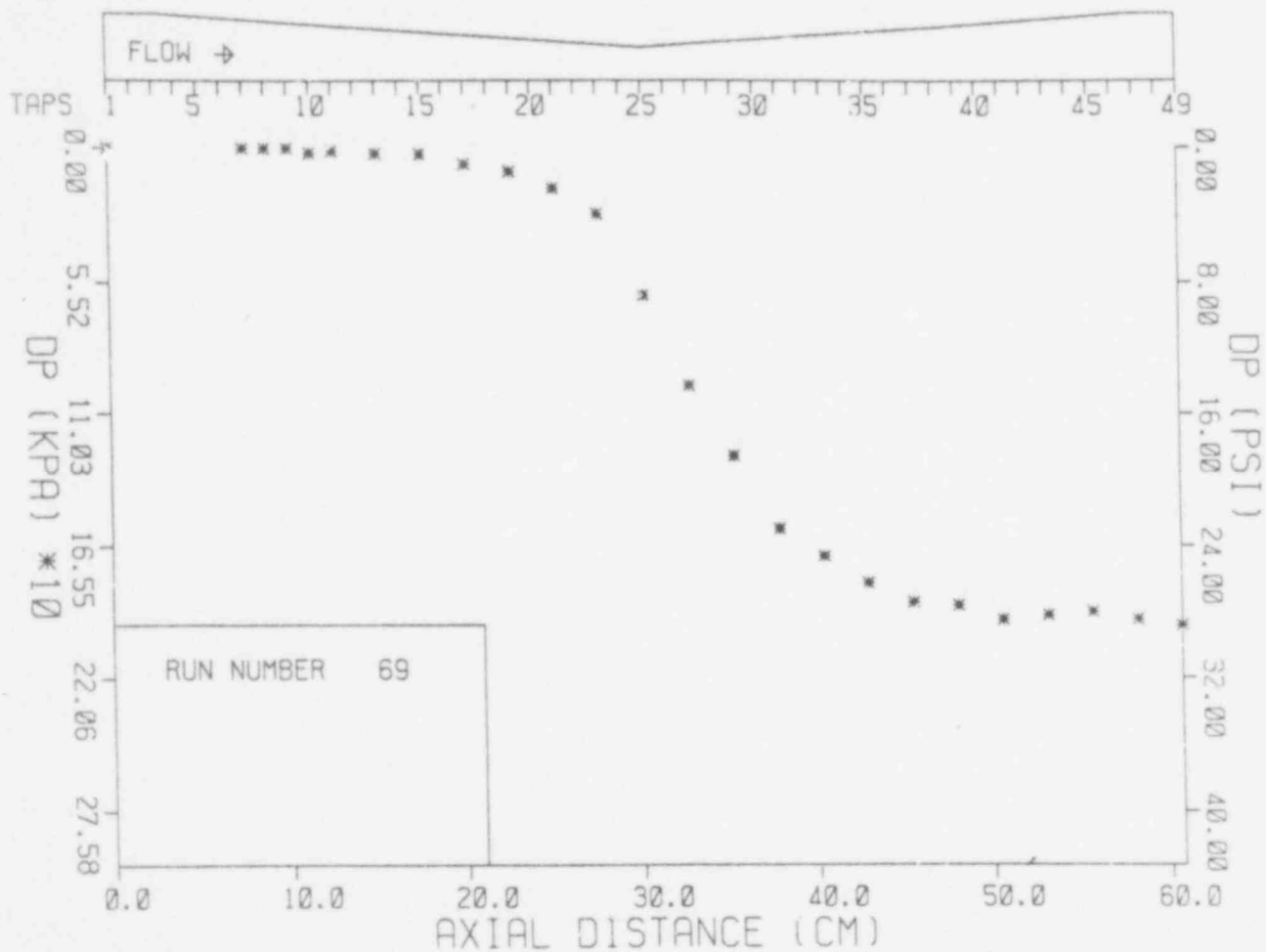


Figure 5.23 Pressure Distributions in the Test Section While Flashing Onset is Upstream of the Nozzle Throat (BNL Neg. No. 3-1024-79)

(5.24). This pressure distribution plot nondimensionalized with the inlet dynamic head of the flow provides an accurate way of determining the onset of vapor generation. For this experiment, it was found that flashing started near pressure Tap 13 (15 cm upstream of the throat).

### 5.3 Void Fraction Measurements Under Flashing Conditions

The axial distributions of the diametrical averaged void fractions were also measured together with the static pressures under various flashing conditions and are presented in this section (Table VI).

#### 5.3.1. Flashing Close to the Throat

Figures (5.25A) and (5.25B) present the results for an inlet temperature and pressure of  $99^{\circ}\text{C}$  and  $394\text{ kPa}$  and a mass flux of  $6.05\text{ Mg/m}^2\text{ s}$ . The pressure profile is constant in the diverging section, and the void profiles follow an almost linear variation in Fig. (5.25B). The (+) symbols are the void fraction data, and the crossed circles in Fig. (5.25B) give the difference between the two-phase and single phase dimensionless pressure distributions. The dimensionless pressure was defined as the local pressure drop divided by the inlet dynamic pressure of the flow.  $DP_m^*$  is the dimensionless local pressure drop with respect to the nozzle inlet measured under flashing conditions and  $DP_c^*$  is the corresponding pressure drop measured during the single phase calibration experiments. The onset of flashing can be determined either from the void fraction measurements or from the point of departure of the dimensionless pressure distribution from the single phase calibration curve.

Reducing the mass flux to  $4.91\text{ Mg/m}^2\text{ s}$  and to  $3.06\text{ Mg/m}^2\text{ s}$  while keeping

RUN	G(Mg/m <sup>2</sup> s)	p <sub>in</sub> (kPa)	T <sub>in</sub> (C)	p <sub>c.t.</sub> (kPa)
69	1.23	399	144.3	188

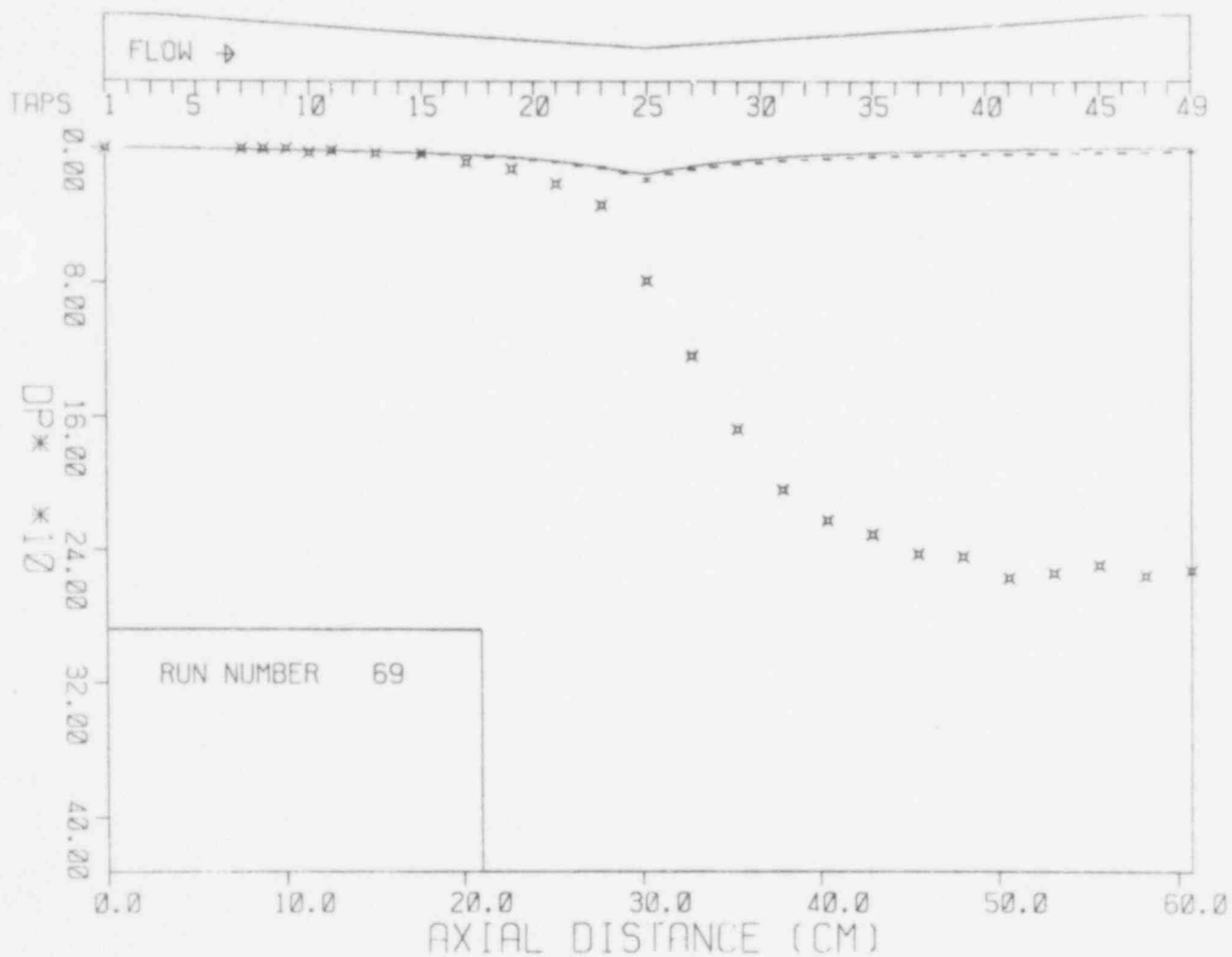


Figure 5.24 Nondimensional Pressure Distribution  $DP^* = DP / \frac{1}{2} \rho U_0^2$   
in the Test Section While the Flashing Onset is  
Upstream of the Nozzle Throat (BNL Neg. No. 3-1026-79)



TABLE VI  
VOID FRACTION DISTRIBUTION DATA  
FLASHING EXPERIMENTS

RUN	$p_{in}$ (kPa)	$T_{in}$ ( $^{\circ}$ C)	$G$ (Mg/m <sup>2</sup> s)	$p_{ct}$ (kPa)	$T_{ct}$ ( $^{\circ}$ C)
730	285	99.4	4.91	54	88.0
740	285	99.4	4.91	54	88.0
762	394	99.3	6.05	61	88.3
770	157	99.3	3.05	67	88.5
771	157	99.3	3.05	67	88.5
780	138	99.3	2.61	71	88.1
781	138	99.3	2.61	71	88.1
792	125	99.4	2.26	76	88.1
793	125	99.4	2.26	76	88.1
801	582	148.3	4.34	434	143.5
802	582	148.3	4.34	434	143.5
812	493	148.3	2.91	431	144.4
813	493	148.3	2.91	431	144.4
821	376	142.3	2.34	175	111.3
822	376	142.3	2.34	175	111.3
831	350	140.0	2.30	147	107.5
832	350	140.0	2.30	147	107.5

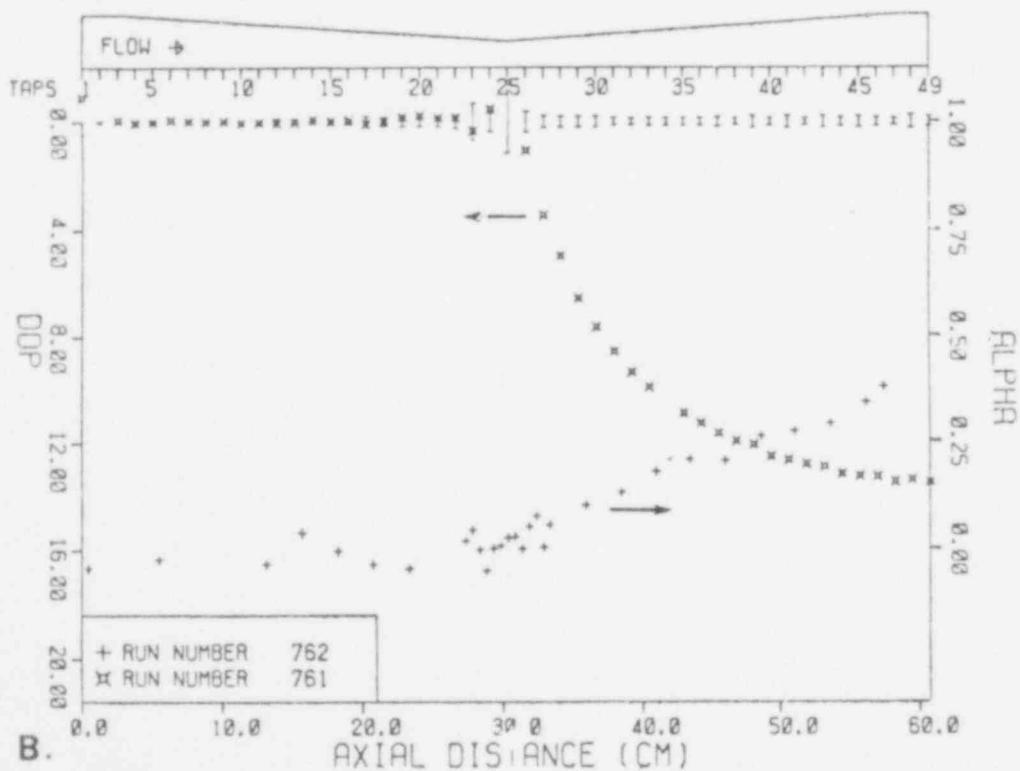
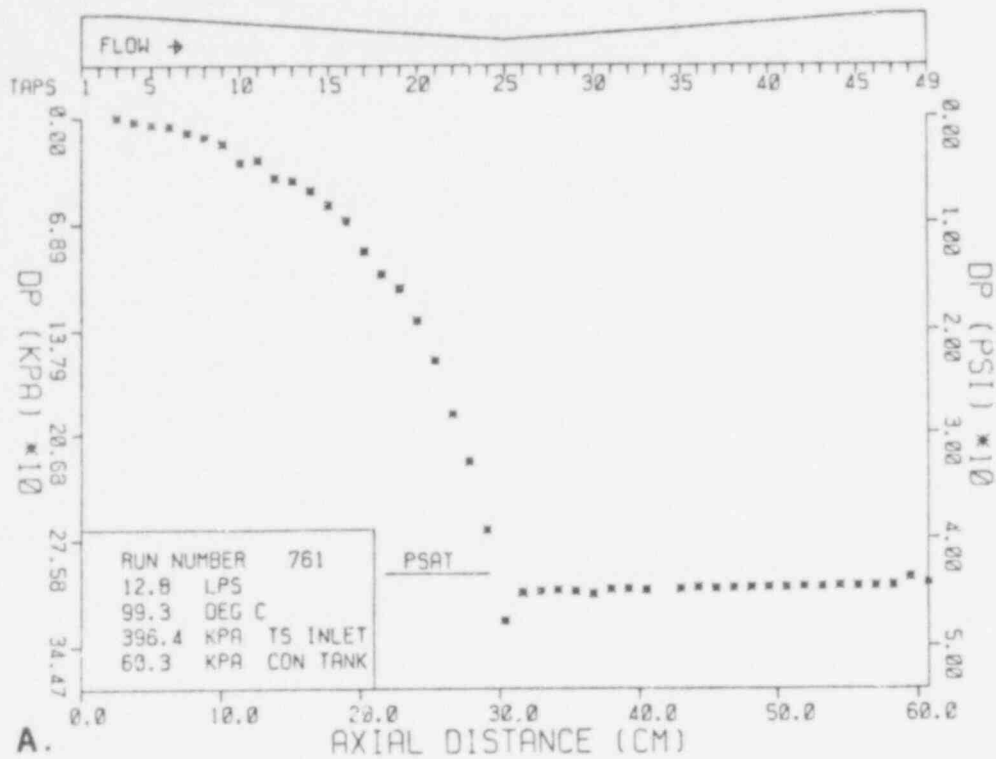


Figure 5.25 Pressure and axial void fraction distributions in the test section. Plot of the difference between the dimensionless measured pressure drop and the nondimensional pressure drop measured in the single phase calibration ( $DDP = DP_m^* - DP_c^{''}$ ) as function of axial distance. (BNL Neg. No. 3-1644-79).

the inlet temperature constant  $\sim 99^{\circ}\text{C}$  we obtained similar results, which are presented in Figs. (5.26) and (5.27). The onset of flashing is close to, but upstream of the nozzle throat. The linear variation of the void fraction with axial distance in the diverging section, combined with the constant pressures observed in Fig. (5.26A) and the fact that the test section diameter also varied linearly, seems to imply the presence of a nearly constant area liquid jet at the core surrounded by a steam envelope. When the mass flux is further reduced to  $3.05 \text{ Mg/m}^2\text{s}$ , the pressure profile in the diverging section starts to show a slight recovery (Fig. 5.27A), which is accompanied in the void fraction profiles by a region where the voids are constant (Fig. 5.27B). If one still reduces the mass flux to  $2.61 \text{ Mg/m}^2\text{s}$ , the pressure distributions observed in Fig. (5.28A), show a sudden pressure recovery in the diverging section which may be considered as a condensation front. This fact is clearly observed in Fig. (5.28B), which shows an increase in the void fraction followed by a decrease to the all liquid situation. The dimensionless profiles of DDP plotted on the same figure also show the pressure deviations from the single phase calibration which closely follow the evaporation and condensation fronts. Still lowering the mass flux to  $2.26 \text{ Mg/m}^2\text{s}$  brings us to a situation which is close to the onset of flashing. Figure (5.29A) depicts the pressure distribution which is very close to the single phase calibration results, and the void fraction distribution presented in Fig. (5.29B) shows a very slight rise close to the throat, but otherwise remains mostly liquid throughout the test section. A similar sequence of events was also observed in experiments at an inlet temperature of  $148.3^{\circ}\text{C}$  for two mass fluxes  $4.34 \text{ Mg/m}^2\text{s}$  (Fig. 5.30A and 5.30B) and  $2.91 \text{ Mg/m}^2\text{s}$  (Fig. 5.31Aa and Fig. 5.31B). The high mass flux

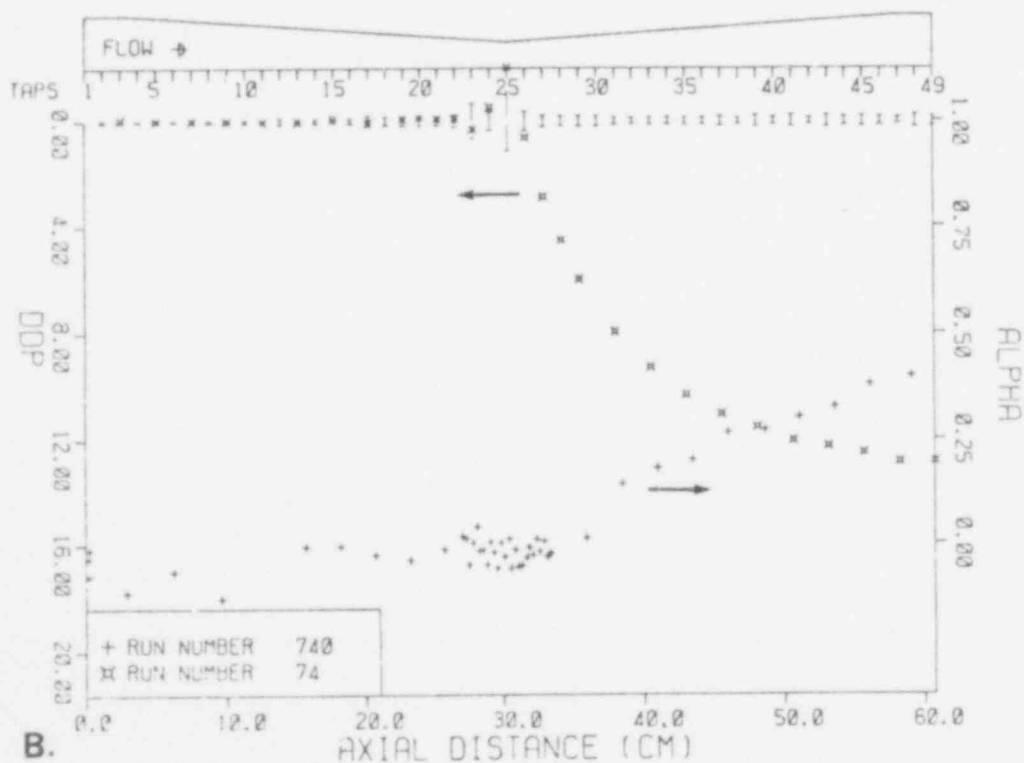
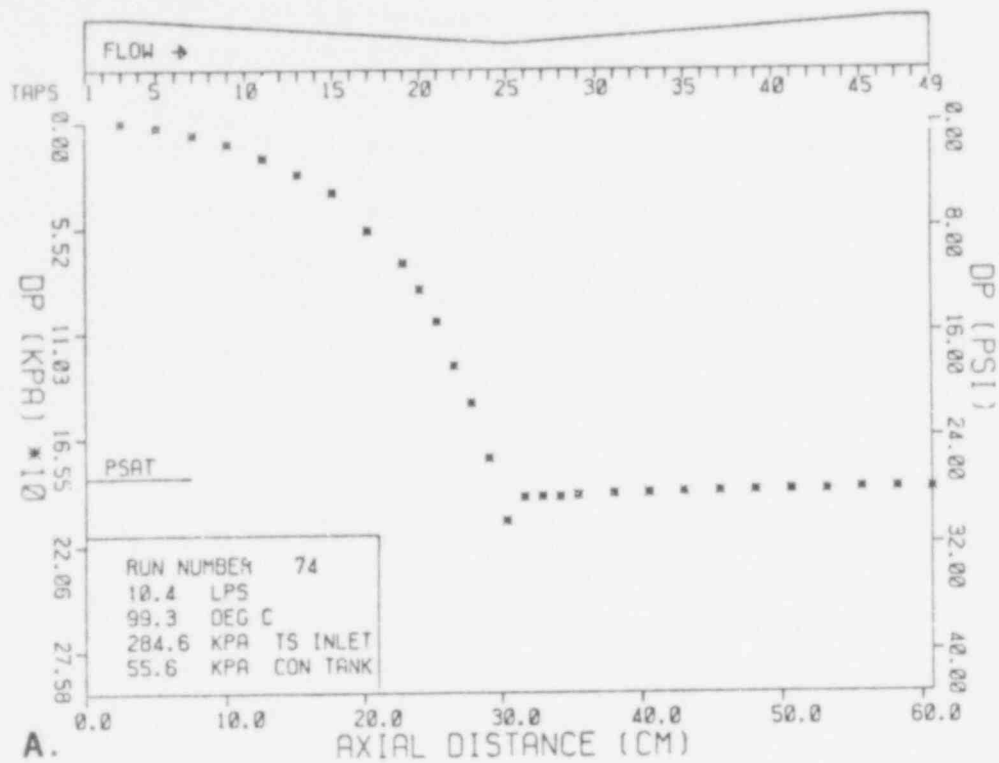
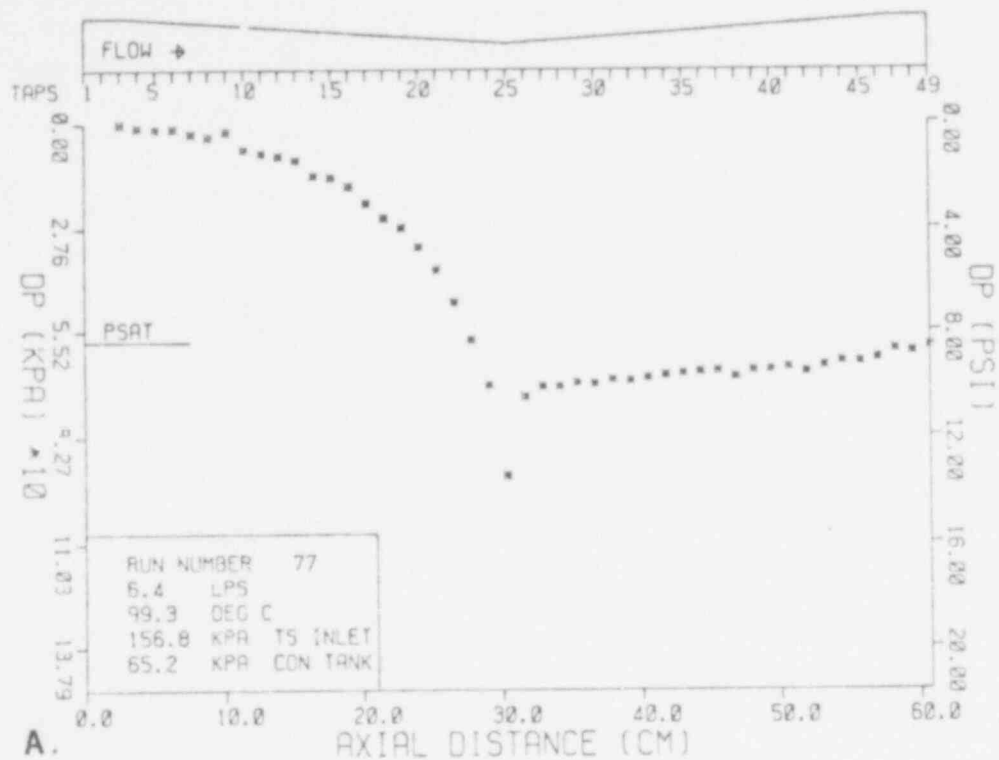
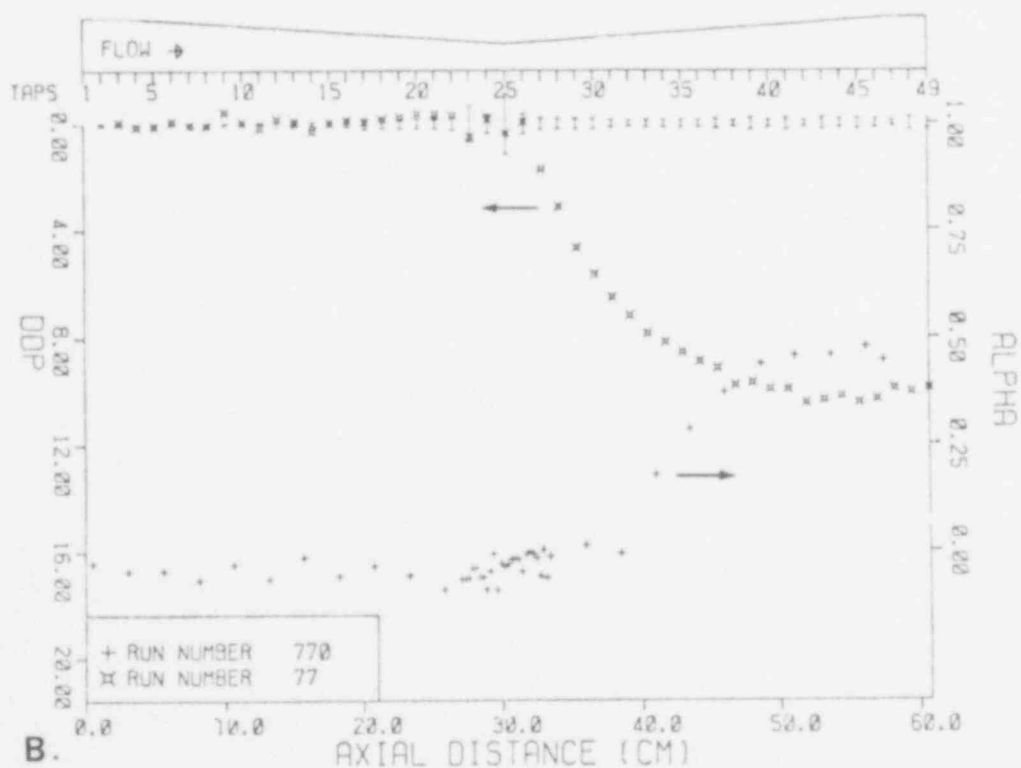


Figure 5.26 Pressure and axial void fraction distributions in the test section. Plot of the difference between the dimensionless measured pressure drop and the nondimensional pressure drop measured in the single phase calibration ( $DDP = DP_m^* - DP_c^*$ ) as function of axial distance. (BNL Neg. No. 3-1645-79).

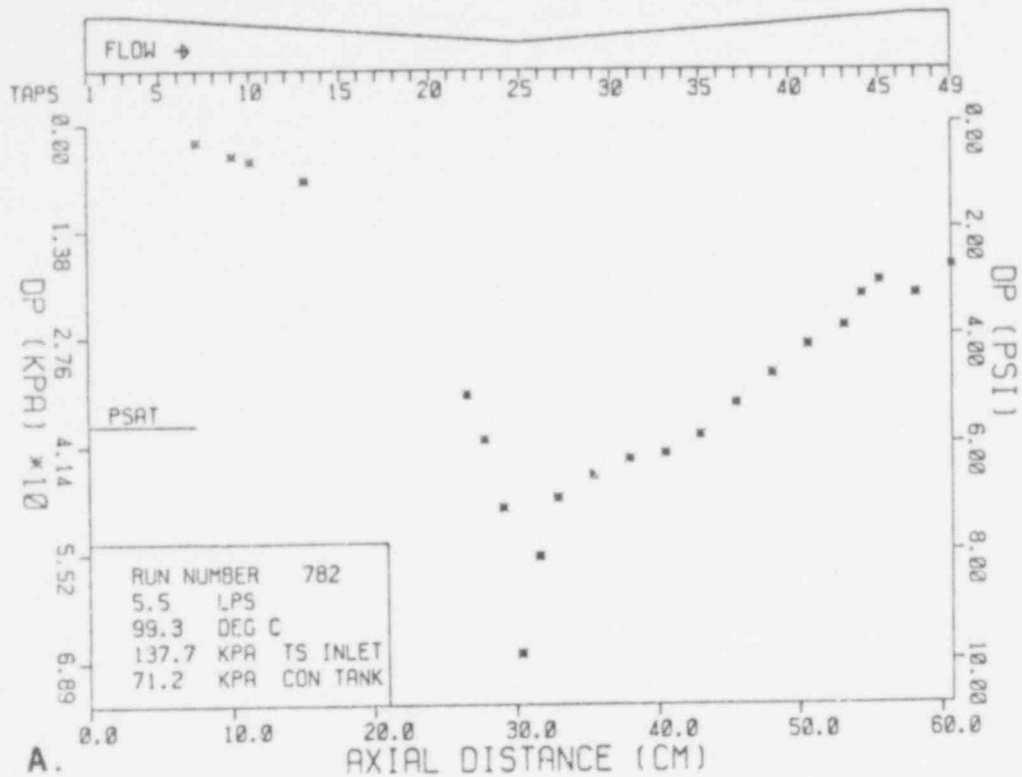


A.

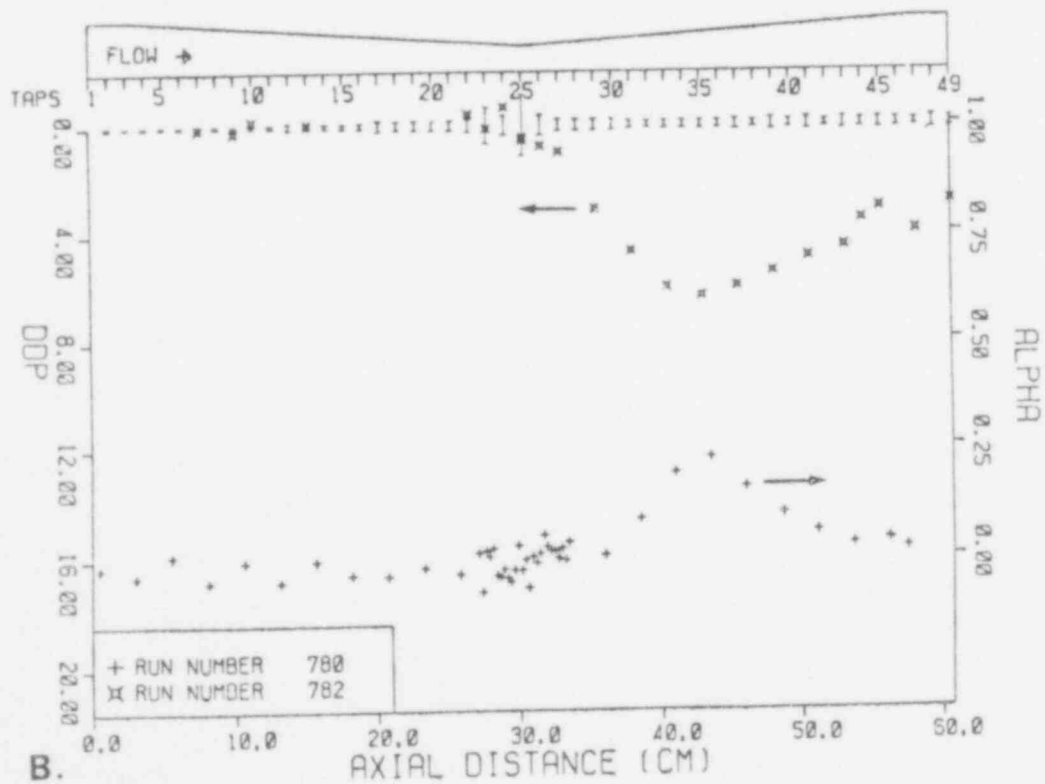


B.

Figure 5.27 Pressure and axial void fraction distributions in the test section. Plot of the difference between the dimensionless measured pressure drop and the nondimensional pressure drop measured in the single phase calibration ( $DDP = DP_m^* - DP_c^*$ ) as function of axial distance. (BNL Neg. No. 3-1643-79).



A.



B.

Figure 5.28 Pressure and axial void fraction distributions in the test section. Plot of the difference between the dimensionless measured pressure drop and the nondimensional pressure drop measured in the single phase calibration ( $DDP = DP_m^* - DP_c^*$ ) as function of axial distance.

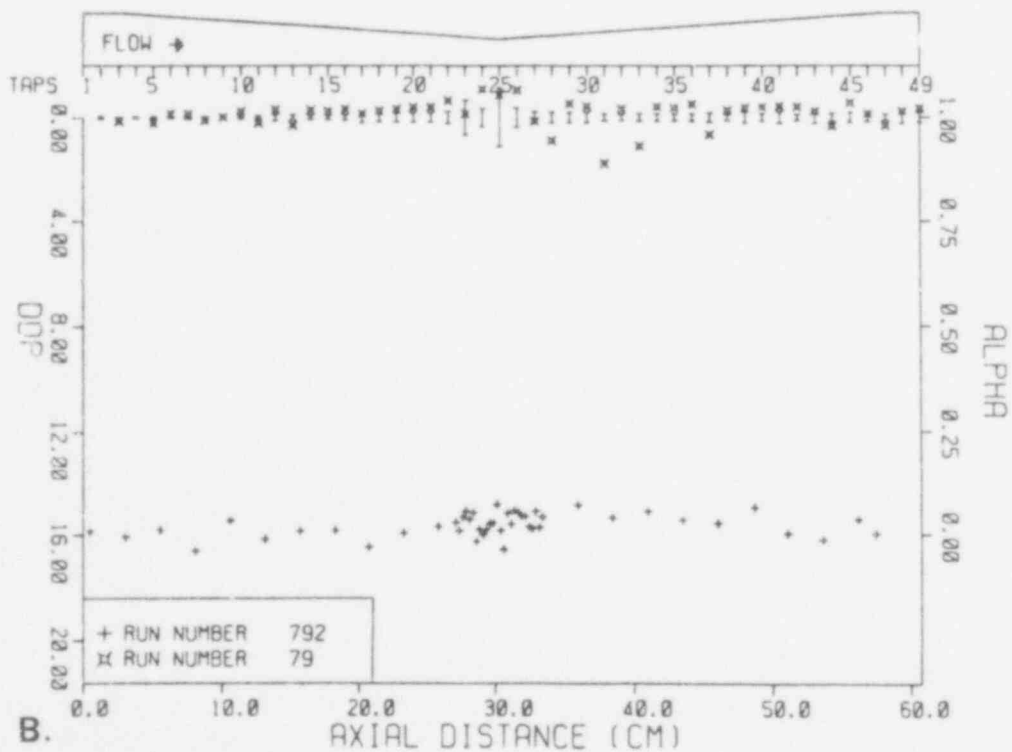
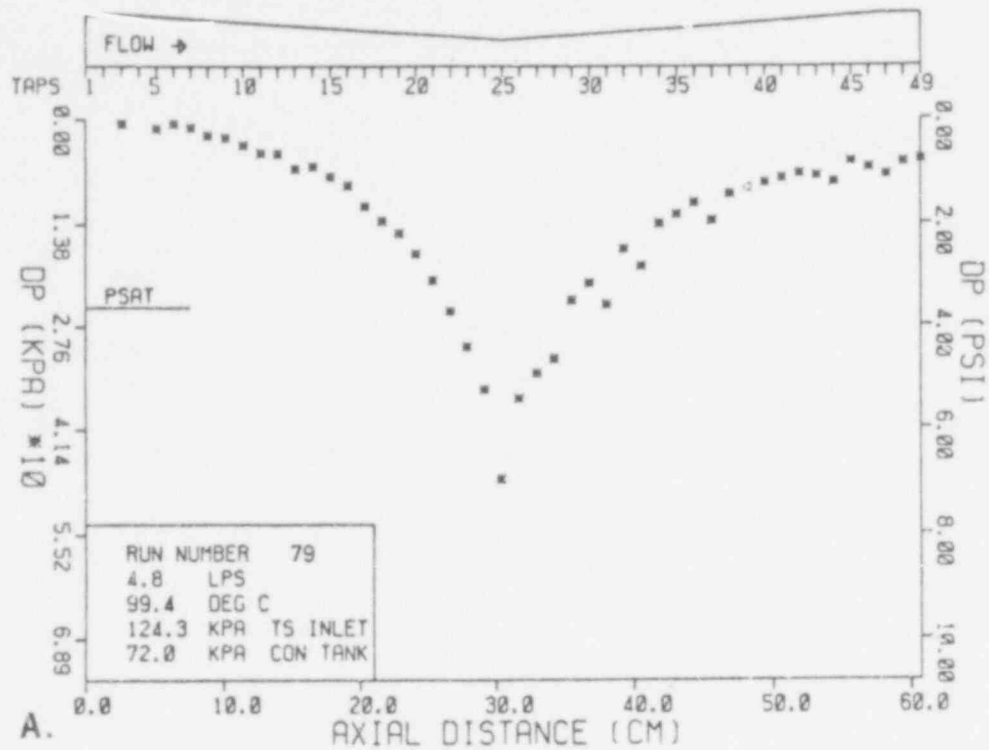


Figure 5.29 Pressure and axial void fraction distributions in the test section. Plot of the difference between the dimensionless measured pressure drop and the nondimensional pressure drop measured in the single phase calibration ( $DDP = DP_m^* - DP_c^*$ ) as function of axial distance.

(BNL Neg. No. 3-1110-79).

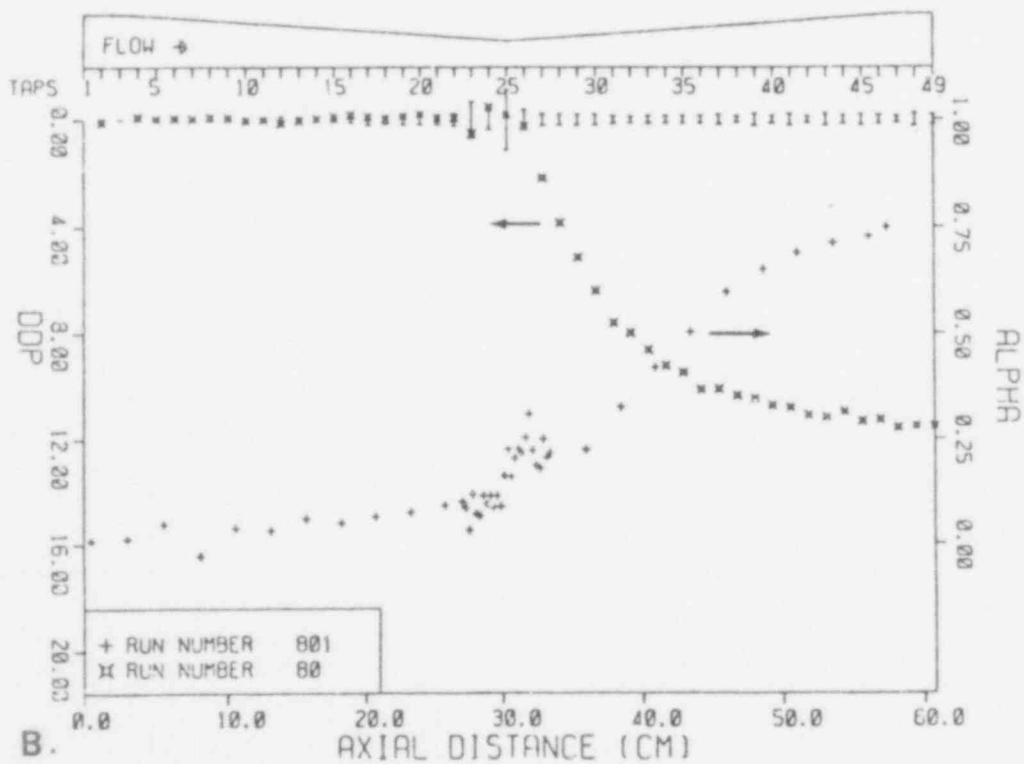
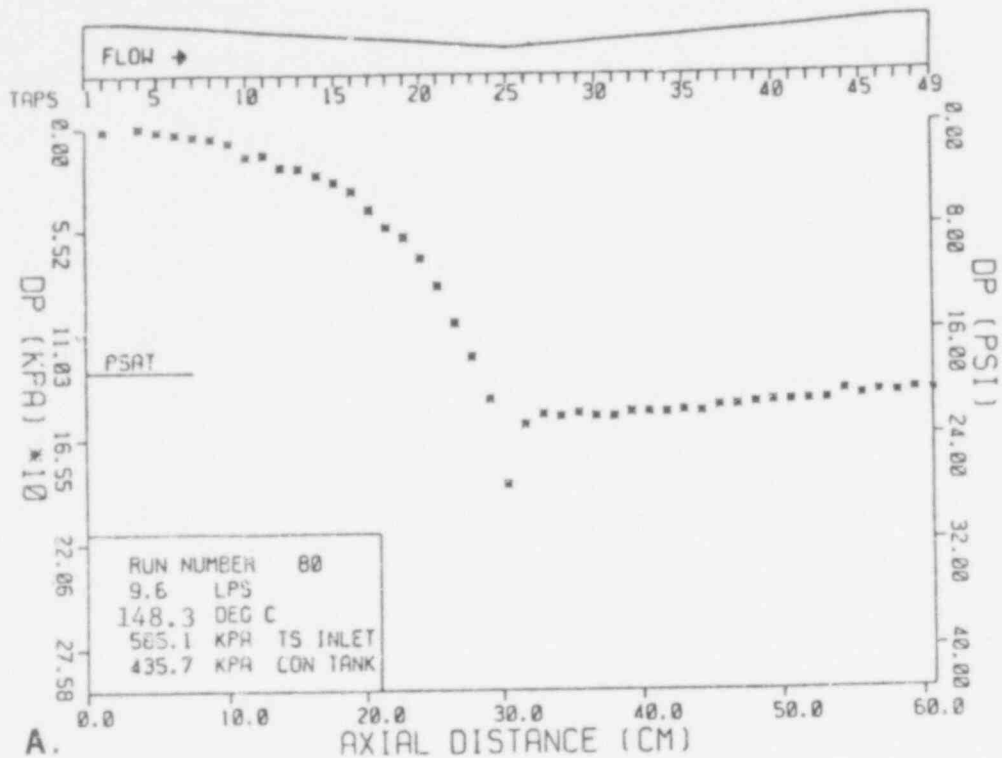


Figure 5.30 Pressure and axial void fraction distributions in the test section. Plot of the difference between the dimensionless measured pressure drop and the nondimensional pressure drop measured in the single phase calibration ( $DDP = DP_m^* - DP_c^*$ ) as function of axial distance.

(BNL Neg. No. 3-1111-79).



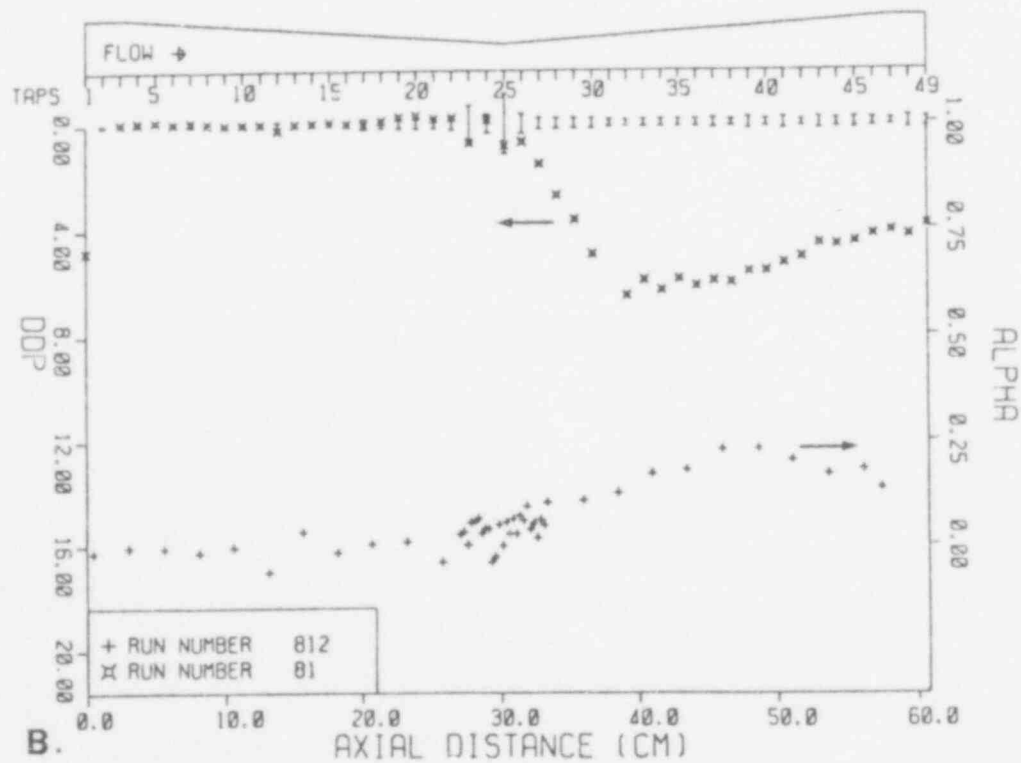
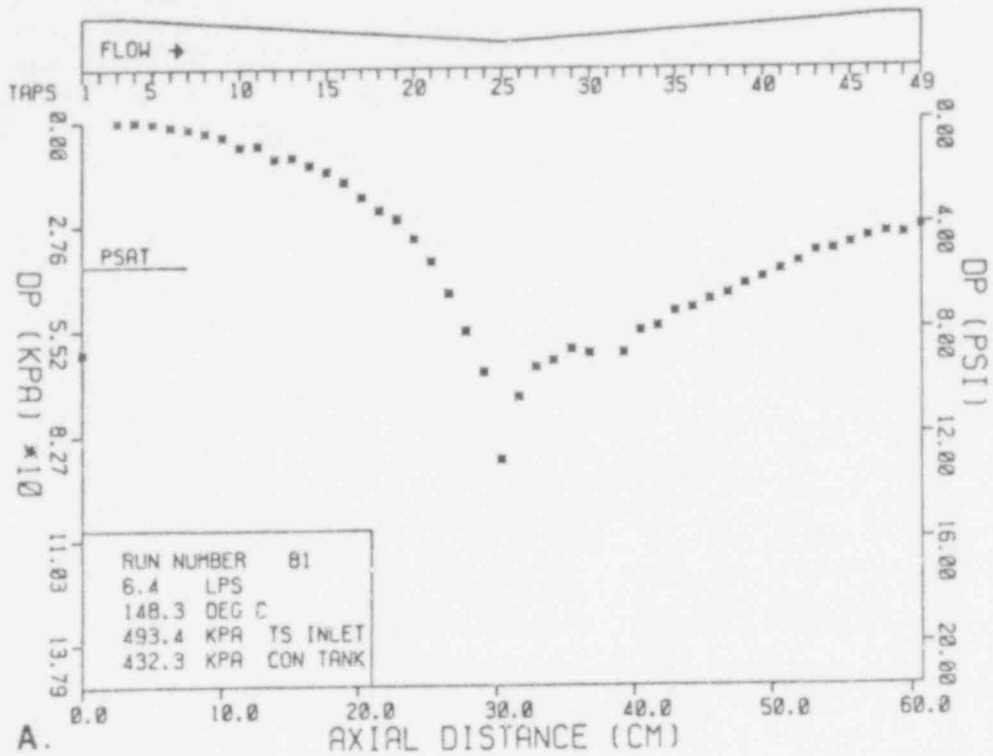


Figure 5.31 Pressure and axial void fraction distributions in the test section. Plot of the difference between the dimensionless measured pressure drop and the nondimensional pressure drop measured in the single phase calibration ( $DDP = DP_m^* - DP_c^*$ ) as function of axial distance.

run presented in Fig. (5.30A) and (5.30B) shows an almost constant pressure distribution in the diverging section with a steeper rise in the void fraction profiles and higher void fraction values at the exit of the nozzle. The 1 : mass flux run presented in Fig. (5.31A) and (5.31B) depicts a vaporization zone in the diverging section downstream of the throat followed by a condensation region which reduces the void fraction (Fig. 5.31b) and causes a pressure recovery close to the test section exit (Fig. 5.31a).

### 5.3.2. Flashing Upstream of the Throat

Additional data was also recorded with the flashing front upstream of the throat. Figures (5.32) and (5.33) present the results for two mass fluxes 2.34 and 2.30  $\text{Mg/m}^2\text{s}$  at an inlet temperature of  $140^\circ\text{C}$ . Figure (5.32A) depicts the pressure distribution for which Fig. (5.32B) presents the void fraction profiles. The pressure distribution shows a decrease in the converging, as well as in the diverging sections of the nozzle. However, the slope seems not to be continuous at the throat in contrast to what is usually presented in the literature. The void fraction profiles show that at the test section inlet, the void fraction was around 10 percent, and the vapor generation increases along the test section, causing a void fraction of almost unity at the exit of the venturi. The DDP plot shows clearly the drastic deviation of the dimensionless pressure profiles from the single phase calibration curve. Figures (5.33A) and (5.33B) present similar results obtained at a mass flux of 2.22  $\text{Mg/m}^2\text{s}$  and an inlet temperature of  $140^\circ\text{C}$ . The results of those two experiments were used to calculate the net vapor generation rates under nonequilibrium conditions, and the methodology followed will be presented in the next section.

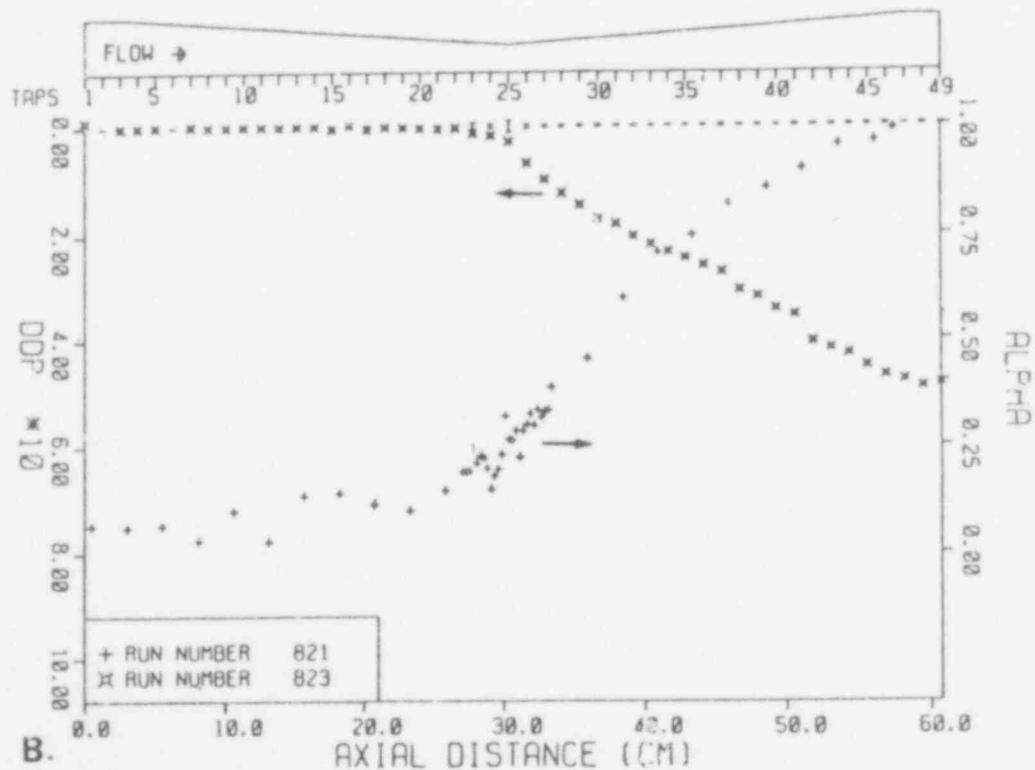
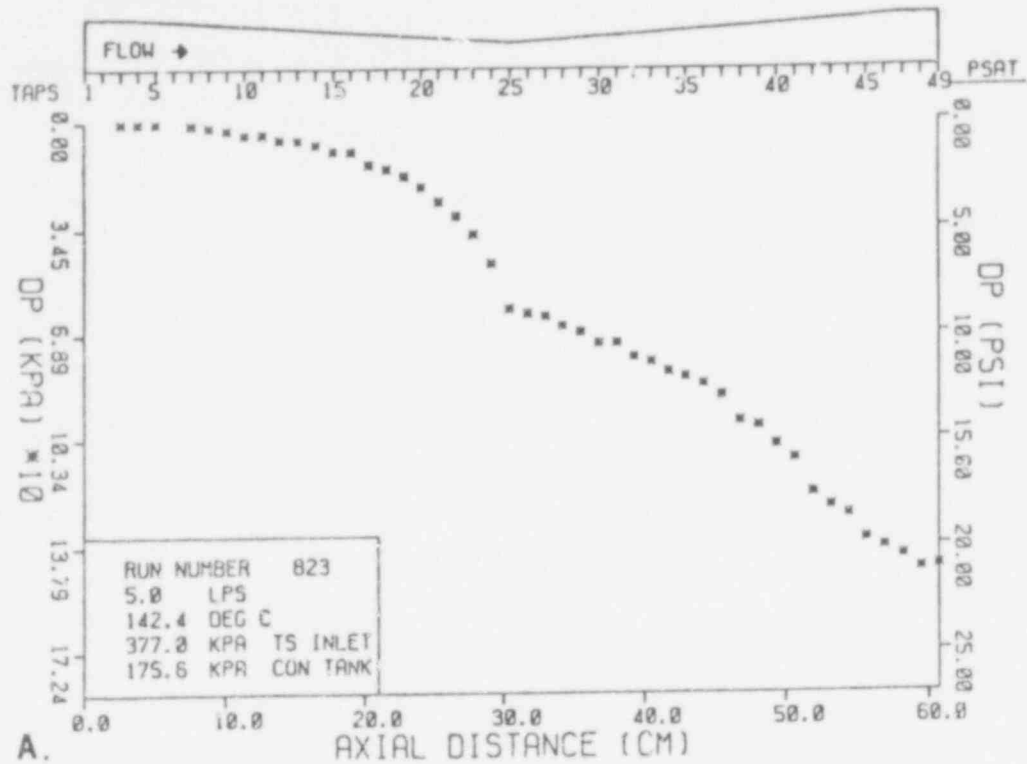


Figure 5.32 Pressure and axial void fraction distributions in the test section with flashing occurring upstream of the nozzle throat. Plot of the difference between the dimensionless measured pressure drop and the nondimensional pressure drop measured in the single phase calibration,

$$(DDP = DP_m^* - DP_c^*) \text{ as a function of axial distance (BNL Neg. No.}$$

3-1108-79).

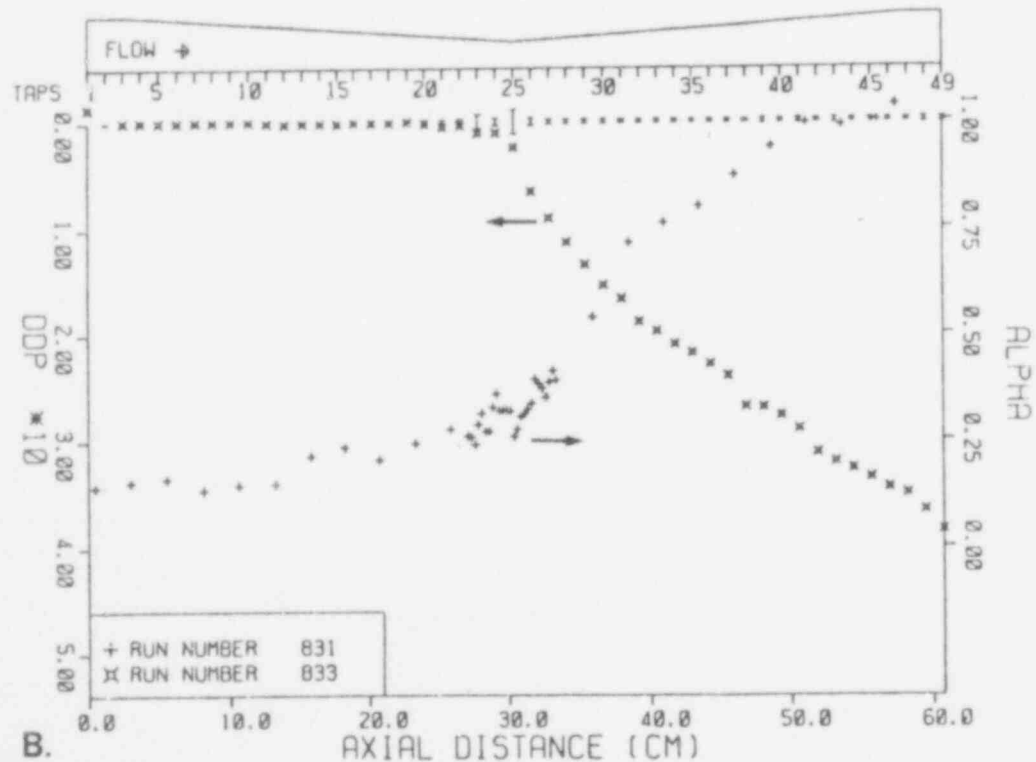
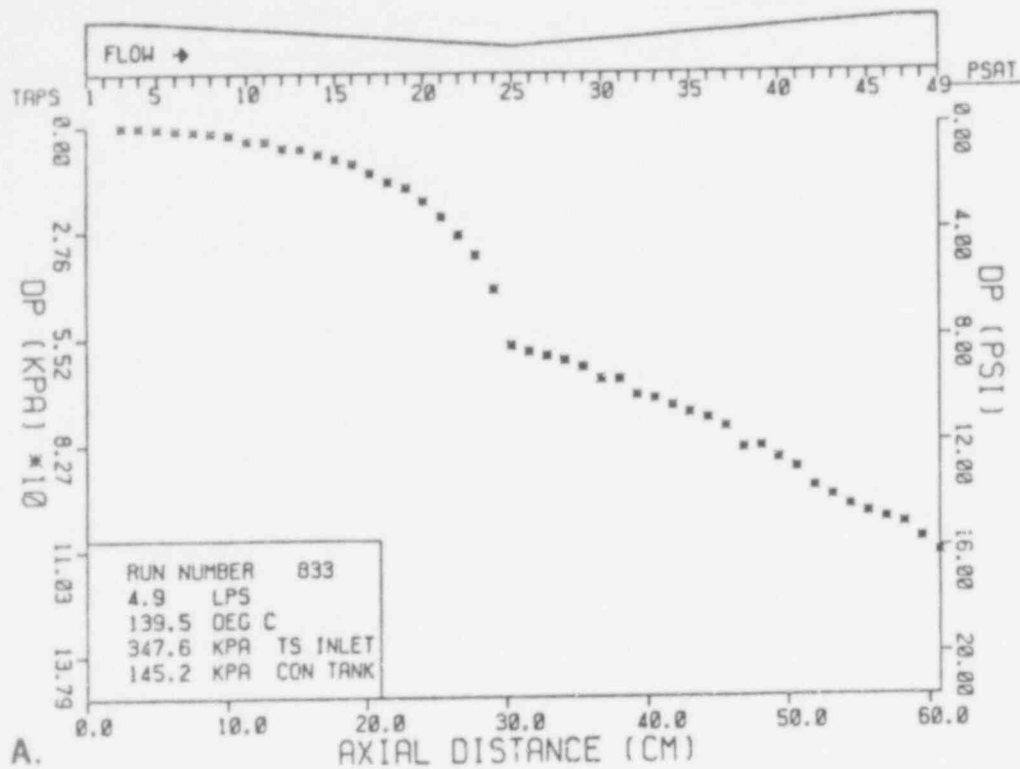


Figure 5.33 Pressure and axial void fraction distributions in the test section with flashing occurring upstream of the nozzle throat. Plot of the difference between the dimensionless measured pressure drop and the nondimensional pressure drop measured in the single phase calibration,  $(DDP = DP_m^* - DP_c^*)$  as a function of axial distance. (BNL Neg. No. 3-1109-79).

#### 5.4 Calculations of Net Vapor Generation Rates Under Flashing Conditions

In this section, we shall present the method with which a cross-section-averaged net vapor generation rate per unit volume  $\Gamma_v$  may be determined from the measured pressure and void fraction distributions along the test section. We recall the following definitions of cross-section-averaged quantities.

Mixture density,

$$\langle \rho \rangle = \langle \alpha \rho_v \rangle + \langle (1 - \alpha) \rho_l \rangle \quad (2)$$

Mass flux of vapor,

$$\langle G_v \rangle = \langle \alpha \rho_v u_v \rangle \quad (3)$$

Liquid mass flux,

$$\langle G_l \rangle = \langle (1 - \alpha) \rho_l u_l \rangle \quad (4)$$

Total mass flux,

$$\langle G \rangle = \langle G_v \rangle + \langle G_l \rangle \quad (5)$$

Total volume flux,

$$\langle j \rangle = \langle \alpha u_v \rangle + \langle (1 - \alpha) u_l \rangle \quad (6)$$

Quality,

$$\langle x \rangle = \langle G_v \rangle / \langle G \rangle \quad (7)$$

We shall assume that the densities  $\rho_v$  and  $\rho_l$  of the vapor and liquid phases are given by the saturation values corresponding to the local pressure  $p$ , and therefore, are constant over a cross-section. Moreover, we

shall assume that the vapor drift velocity

$$V_{gj} = u_v - j \quad (8)$$

is also constant over a cross-section. Combining Eqs. (7) and (3) and using the drift velocity, Eq. (8) we have

$$\begin{aligned} \langle x \rangle \langle G \rangle &= \langle \alpha \rho_v j \rangle + \langle \alpha \rho_v V_{gj} \rangle \\ &= \rho_v (\langle \alpha j \rangle + \langle \alpha \rangle V_{gj}). \end{aligned} \quad (9)$$

Introducing the distribution parameter  $C_o = \langle \alpha j \rangle / \langle \alpha \rangle \langle j \rangle$ , we may write

$$\langle x \rangle \langle G \rangle = \rho_v (C_o \langle \alpha \rangle \langle j \rangle + \langle \alpha \rangle V_{gj})$$

which may be expressed as

$$\langle x \rangle \langle G \rangle = \rho_v \langle \alpha \rangle \left[ C_o \left( \frac{\langle x \rangle \langle G \rangle}{\rho_v} + \frac{\langle 1 - x \rangle \langle G \rangle}{\rho_l} \right) + V_{gj} \right],$$

when Eqs. (6), (3), and (4) are inserted. Solving for the cross-section-averaged quality  $\langle x \rangle$  and replacing the liquid and vapor densities with their saturation values, we get finally

$$\langle x \rangle = \frac{\langle \alpha \rangle \left[ C_o \frac{\rho_g}{\rho_f} + \frac{\rho_g V_{gj}}{\langle G \rangle} \right]}{1 - \langle \alpha \rangle C_o \frac{\rho_f - \rho_g}{\rho_f}} \quad (10)$$

The vapor drift velocity is assumed to be given by the expression for the churn-turbulent upflow of a bubbly mixture,

$$V_{gj} = K \left[ \frac{\sigma g (\rho_f - \rho_g)}{\rho_f^2} \right]^{1/4} \quad (11)$$

where the coefficient  $K = 1.41$  according to Kroeger and Zuber (1968). For a given set of test section inlet conditions, we may assume that  $C_o$  remains constant in the test section, and that the variation of the liquid density  $\rho_f$  is negligible. Thus  $V_{gj}$  varies only weakly with  $\rho_g$ , and we shall assume  $V_{gj}$  to be roughly constant in the test section as well. Hence  $\langle x \rangle$  may be considered as an explicit function of the local cross-section averaged void fraction, the vapor density and mixture mass flux.

From conservation of vapor mass, we have

$$\Gamma_v = \langle G \rangle d\langle x \rangle / dz \quad (12)$$

which leads to, after dropping the symbol  $\langle \rangle$ ,

$$\Gamma_v = \frac{\frac{Gx}{\alpha} \frac{d\alpha}{dz} + \frac{Gx}{\rho_g} (1 - \alpha C_o) \frac{d\rho_g}{dp} \frac{dp}{dz} - \frac{\alpha \rho_v}{G} \frac{V}{g} \frac{dG}{dz}}{1 - \alpha C_o (\rho_f - \rho_g) / \rho_f} \quad (13)$$

where we have replaced  $d\rho_g/dz$  by  $[(d\rho_g/dp)(dp/dz)]$ . The quantities  $da/dz$  and  $dp/dz$  in Eq. (13) may be obtained from the experiments, and  $d\rho_g/dp$  is given by the equation of state of the vapor, or the steam table. We note, from the mixture continuity equation

$$\frac{1}{G} \frac{dG}{dz} = - \frac{1}{A} \frac{dA}{dz} = - \frac{1}{(A/A^+)} \frac{d(A/A^+)}{dz} \quad (14)$$

To account for the frictional effects in an approximate manner, the effective cross-sectional area distribution  $(A/A^+)_{\text{eff}}$  determined from single phase calibrations instead of the geometrical area distribution were used in the reported calculations. This is probably a good assumption in the convergent section where the favorable pressure gradient is expected to keep the wall boundary layers thin and attached. Greater uncertainty arises when such a procedure is applied to the divergent part of the test section where the boundary layer displacement in two-phase flow may be significantly different from the single-phase flow under adverse pressure gradients. Thus, all terms in Eq. (13) may be evaluated as a function of  $z$  and the net vapor generation rate may be calculated.



Figures (5.34) and (5.35) show the two examples of  $\Gamma_v$  thus determined for the convergent part of the test section. In these figures, the top graph displays the measured pressure and void distributions in the experiments. In addition, least-square polynomial fits to the measured data are also shown for comparison. The derivatives of  $\alpha$  and  $p$  may be evaluated along the fitted polynomials, instead of through the actual data points, which may lead to considerable scatter. The  $\Gamma_v$  values calculated from Eq. (13) are exhibited in the bottom graphs.\* It is seen that  $\Gamma_v$ 's of the order of  $10^2$   $\text{kg/m}^3\text{s}$  are attained in these experiments, which are in approximately the same range as those found in Reocreux's (1974) experiments.

It was found that the value of  $\Gamma_v$  was dominated by far by the variation of  $\alpha$  with  $z$  in these experiments. For example, for Runs 82/821 at  $z = 254$  mm, the value of the three terms in the numerator in Eq. (13) are

$$(Gx/\alpha)d\alpha/dz = 22.53 \text{ kg/m}^3\text{s},$$

$$(Gx/\rho_g)(1 - \alpha C_o)(d\rho_g/dp)(dp/dz) = - 2.66 \text{ kg/m}^3\text{s},$$

$$(\alpha\rho_g V_{gj}/G)dG/dz = 0.33 \text{ kg/m}^3\text{s},$$

where  $V_{gj} = 0.21$  m/s.

Thus, the term involving  $dG/dz$ , which is directly proportional to the drift velocity assumed, contributes about one percent to the value of  $\Gamma_v$ . Any uncertainty in the assumption of  $V_{gj}$  is expected to lead to insignificant

\* In Fig. (5.35), the sudden turn in the  $\Gamma_v$  curve at  $z \approx 260$  mm may be traced back to the discontinuity in the slope of the two pieces of 3-deg. polynomial fit to the experimental data at the intersection of the two polynomials. For this preliminary evaluation of data, a better curve fit, which may yield a smoother transition from one polynomial to another has not been attempted.

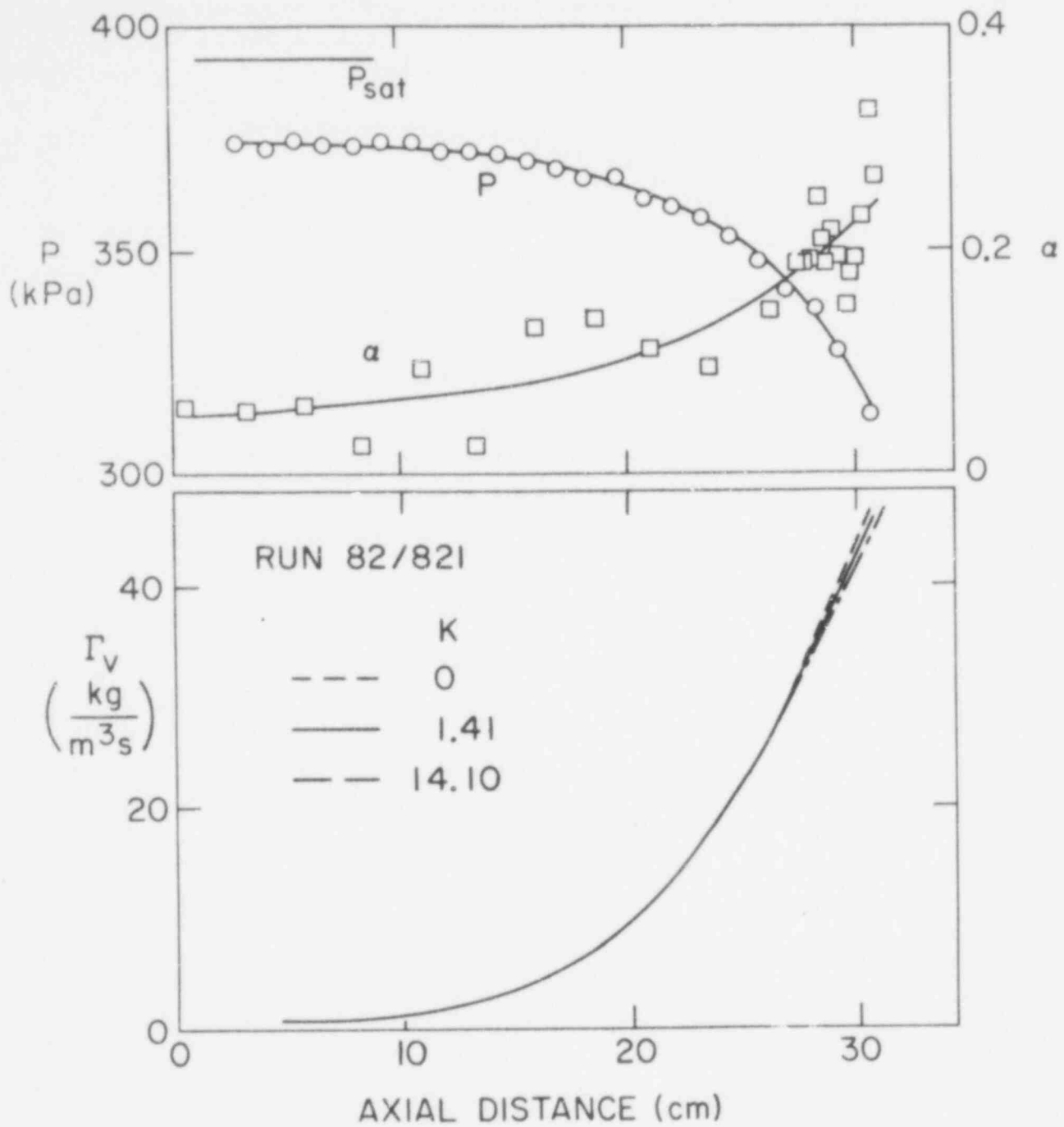


Figure 5.34 Top: Measured Pressure (o) and Void Fraction (□) Distributions in the Converging Part of the Test Section in Runs 82/821 and the Least Square Polynomial Fit to Data. Bottom: Calculated Net Vapor Generation Rate Based on the Least Square Fit to the  $\alpha$  and  $p$  Data. (BNL Neg. No. 3-1226-79).

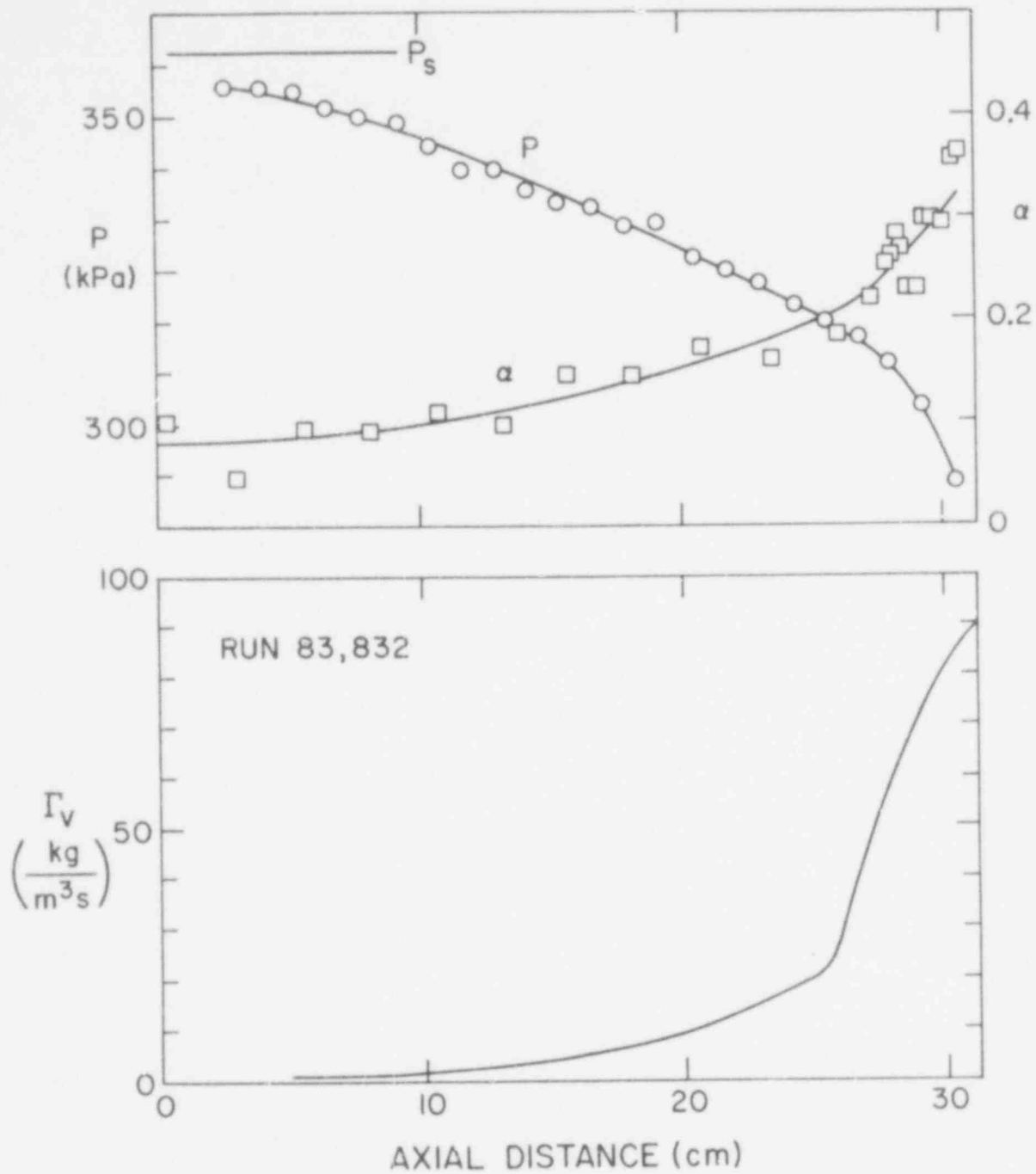


Figure 5.35 Top: Measured Pressure (o) and Void Fraction (□) Distributions in the Converging Part of the Test Section in Runs 83/832 and the Least-Square Polynomial Fit to the Data. Bottom: Calculated Net Vapor Generation Rate Based on the Least-Square Fit to the  $\alpha$  and  $p$  Data. (BNL Neg. No. 3-1225-79).

errors in  $\Gamma_v$  thus determined. In Fig. (5.34), we have also shown  $\Gamma_v$ 's calculated for zero drift velocity and a ten-fold increase in  $V_{gj}$  (taking  $K = 0$  and 14.1, respectively, in Eq. (11)). The difference between the three curves are indeed small. Hence, it may be concluded that void fraction and pressure distribution measurements are adequate for the determination of cross-section averaged vapor generation rates.

## 6. SUMMARY AND CONCLUSIONS

In order to measure the steady state vapor generation rates under nonequilibrium conditions, a flow loop with well controlled flow and thermodynamic conditions was designed, built and made operational. The test section consisting of a converging-diverging nozzle was first calibrated hydrodynamically with single phase flows. Pressure distributions were recorded along the test section and photographic observations made at the exit of the test section under various flashing regimes. With flashing occurring close to, but upstream of the throat, the pressure distribution in the converging section was observed to follow closely the single phase calibration results. In the diverging section of the nozzle, either a continuous constant pressure distribution was observed all along this region or the constant pressure was followed by a sudden pressure increase (condensation shock) and a single phase-like pressure recovery.

Variation of the back pressure revealed a choked flow pattern in the converging section of the nozzle. Depending on the back pressure, the pressure distributions in the diverging sections showed the presence of a condensation shock. In the absence of condensation shocks in the test

section, marked variations were seen in the photographic observations at different back pressures, but corresponding variations were not observed in pressure distributions.

During the investigation of the parametric effects, the mass flux and inlet pressures were found to have a stronger effect on the pressure distributions and photographic observations than variations in the inlet temperatures under constant  $p_{in} = p_{sat}(T_{in})$  conditions. These parametric effects were more visible at low mass fluxes at the onset of flashing than at higher ones. The flashing onset was also observed to be an intermittent phenomenon.

Flashing was also initiated upstream of the nozzle throat, and the pressure distributions depicted a continuous decrease in the converging, as well as diverging section. The onset of flashing was accompanied with a strong deviation in the pressure distribution as compared to the single phase calibration.

Using a single beam  $\gamma$ -densitometer, the axial distributions of the diametrical averaged void fractions were measured and compared to the static pressure measurements performed under the same conditions. At high mass fluxes with flashing occurring close to the throat, the constant pressure distributions in the diverging section of the nozzle were accompanied by a linear increase in the void fraction. Since the test section diameter changed linearly, it is suggested that a constant diameter liquid jet existed in the diverging section. At lower mass fluxes, the constant pressure distribution was followed by a pressure recovery. The corresponding void fraction profiles depicted an  $\alpha$ -increase reaching a maximum,

then decreasing to zero, i.e., an air-liquid condition. This fact shows the presence of a condensation region in the diverging section.

Also reported were void fraction profiles with the flashing front well upstream of the nozzle throat. These measurements combined with the pressure distributions were used in calculating the net vapor generation rates under flashing conditions in the converging section of the nozzle. The  $\gamma$  densitometry system will be improved for the next series of experiments, by increasing the strength of the source, thereby increasing the number of counts per unit time to minimize the intrinsic statistical error. In addition, radial profiles will be recorded. Experiments will be conducted according to a proposed matrix, which includes given ranges of the various parameters of interest, i.e.,  $p_{in}$ ,  $T_{in}$ ,  $G$ , and onset of flashing.

#### 7. ACKNOWLEDGEMENTS

The authors would like to thank all the members of the Data Systems and Operations Group, namely Messrs. James H. Klein, John R. Klages, Carl E. Schwarz, John J. Barry, and Donald Becker for their valuable help during the construction and operation of the experimental facility and to Mr. Thomas P. Feierabend for his essential contributions in the electronic instrumentation.

Special appreciation is due to Ms. Nancy Schneider for typing the manuscript and for her efforts in preparing the report.

Our thanks to William Messenger of the welding shop for his imagination and dedication in putting the pieces together and to Dennis Rhodes and Edward McGilley of the electrical shop who ingeniously sorted out the

maze of electrical connections and made the pumps pump. We would also like to express our gratitude to Eugene C. Mohlmann for the expeditious manner in which he handled our rush orders, and specially to Herb Banks for his invaluable help with our purchases and negotiations with the various vendors. Dr. Hobart W. Kraner's suggestions, help and guidance on the  $\gamma$ -source and  $\gamma$ -densitometer development were also most welcome at critical moments and are well appreciated.

## 8. REFERENCES

1. Hsu, Y. Y., "Review of Critical Flow, Propagation of Pressure Pulse and Sonic Velocity," NASA TND-6814, 1972.
2. Seha, P., "Review of Two-Phase Steam-Water Critical Flow Models With Emphasis on Thermal Nonequilibrium," NUREG/CR-0417, BNL-NUREG-50907, 1978.
3. Seynhaeve, J. M., "Critical Flow Through Orifices," Paper presented at the European Two-Phase Flow Group Meeting, Grenoble, 1977.
4. Isbin, H. S., Moy, J. E., and DaCruz, A.J.R., "Two-Phase Steam-Water Critical Flow," AIChE J3, 361, 1957.
5. James, R., "Steam-Water Critical Flow Through Pipes," Proc. Instn. Mech. Engrs., 176, 2, 741-748, 1962.
6. Ardron, K. H. and Ackerman, M. C., "Studies of the Critical Flow of Subcooled Water in a Pipe," Paper presented at the CSNI Specialist Meeting on Transient Two-Phase Flow, Paris, 1978.
7. Reocreux, M. and Seynhaeve, J. M., "Ecoulements diphasiques eau-vapeur: essais comparatifs de debits critiques," Acta Technica Belgica EPE Vol X, 3-4, 115-137, 1974.
8. Fauske, H. K., "The Discharge of Saturated Water Through Tubes," Chem. Eng. Prog. Sym. Ser., 61, 210-216, 1965.
9. Reocreux, M., Contribution a l'etude des debits critiques en ecoulements diphasiques eau-vapeur, These de Doctorat, Universite Scientifique et Medicale de Grenoble, 1974.
10. Silver, R. S., "Temperature and Pressure Phenomena in the Flow of Saturated Liquids," Proceedings of the Royal Society of London, Series A, Vol. 194, 17, 1948.
11. Zaloudek, F. R., "The Critical Flow of Hot Water Through Short Tubes," HW-77594, 1963.
12. Fauske, H. K. and Henry, R. E., "The Two-Phase Critical Flow of One-Component Mixtures in Nozzles Orifices and Short Tubes," J. of Heat Transfer, 464, 1971.
13. Schrock, V. E., Starkman, E. S., and Brown, R. A., "Flashing Flow of Initially Subcooled Water in Convergent Divergent Nozzles," presented at the ASME-AIChE Heat Transfer Conference, St. Louis, MO, 1976.



REFERENCES (Cont'd)

14. Simoneau, R. J., "Pressure Distribution in a Converging-Diverging Nozzle During Two-Phase Choked Flow of Subcooled Nitrogen," NASA TMX-71762, 1975.
15. Hendricks, R. C., Simoneau, R. J., and Burrows, R. F., "Two-Phase Choked Flow of Subcooled Oxygen and Nitrogen," NASA TN D-8169, 1976.
16. Reactor Physics Constants, ANL-5800, 1963.
17. Kroeger, P. G. and Zuber, N., "An Analysis of the Effects of Various Parameters in the Average Void Fractions in Subcooled Boiling," Int. J. Heat Mass Transfer, 11.211, 1968.

NOTES TO THE APPENDICES

1. In Runs 1-36, run average values of the flow rate, the test section inlet temperatures and pressures, the condensing tank temperatures and pressures, as well as the turbine flow meter temperatures were hand inputted, and thus they do not show any variations during the experiment.
2. In Runs 20-43, run average values of the flow rate, the test section inlet temperatures and pressures, the condensing tank temperatures and pressures, as well as the turbine flow meter temperatures were hand inputted, and thus they do not show any variations during the experiment.
3. In Runs 44-69, run average values of the test section inlet and condensing tank pressure were hand inputted, and thus they do not show any variations during the experiment.
4. The Differential Pressure Measured in in (kPa) and can be expressed as:

Differential Pressure Measured = DP(kPa)

$$DP(\text{kPa}) = P_{\text{Nth Tap}} + \rho g Z_{\text{Nth Tap}} - P_{\text{Tap 1}}$$

Thus to obtain the local static pressure at every tap, one has to subtract the gravitational head from the presented data.  $\rho$  is the average density in the manifold ( $\sim$  Room Temperature).

5. The dimensionless pressure differential is defined as the differential pressure measured divided by the test section inlet dynamic pressure.

$$DP^* = DP / \frac{1}{2} \rho U_0^2$$

$\rho$  is the density, and  $U_0$  is the velocity at the test section inlet.

LEGEND FOR DATA PRESENTED

SNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER 64

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	9.63	138.0	148.8	148.8	609.2	464.7	474.0	.117E+07	.09	.01
1-4	9.62	138.0	148.7	148.7	609.2	464.7	473.8	.117E+07	.79	.08
1-5	9.61	138.0	148.7	148.7	609.2	464.7	473.5	.117E+07	2.10	.20
1-7	9.62	138.0	148.7	148.7	609.2	464.7	473.9	.117E+07	5.04	.49

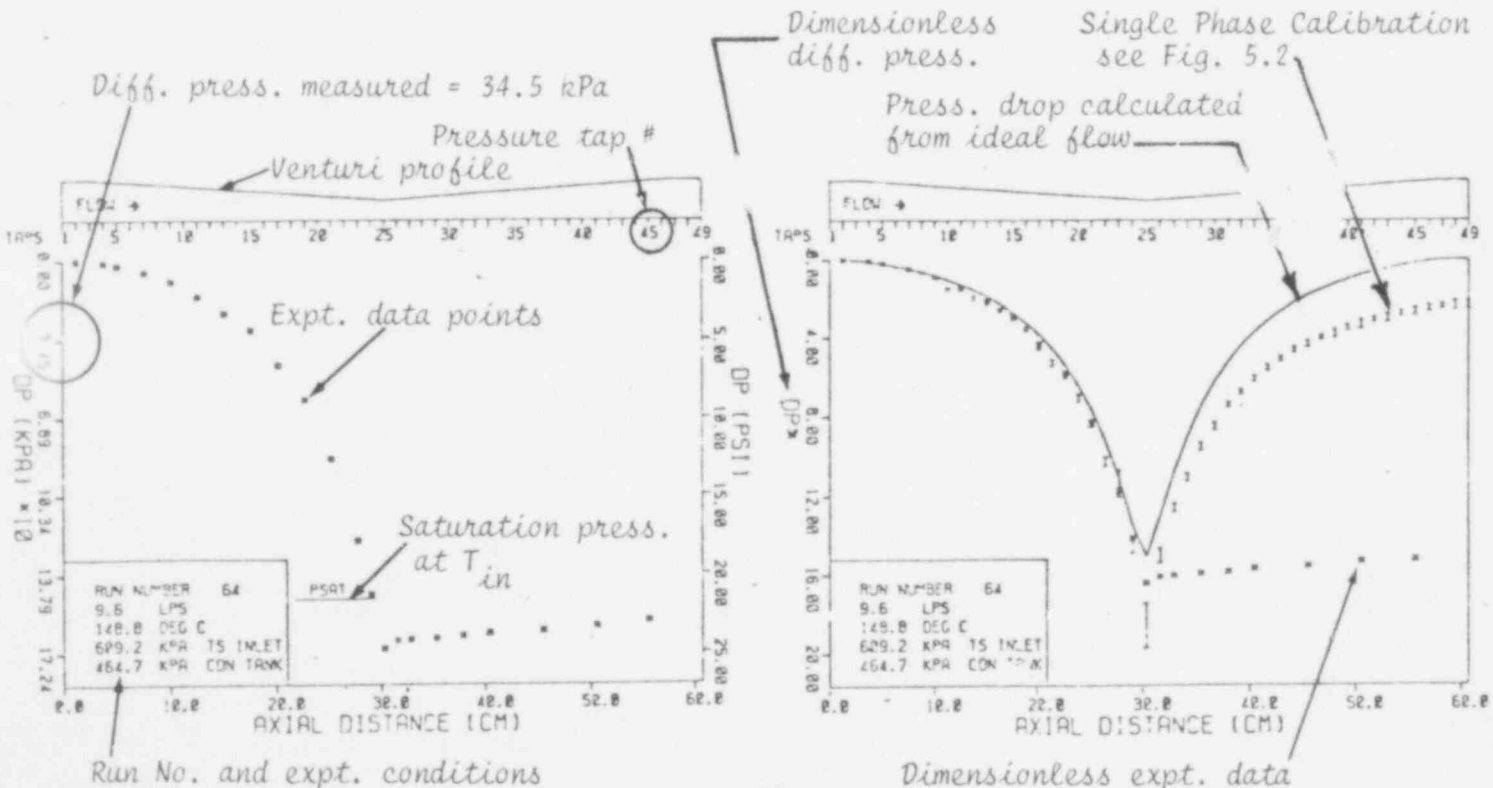
Low press. side  
High press. side

Evaluated at  
Test Section  
Inlet

Diff. press.  
in kPa  
(including  
gravity head  
see p. 15)

Diff. press. nondimensionalized  
by inlet dynamic pressure.

**POOR ORIGINAL**



APPENDIX A

SINGLE PHASE CALIBRATION DATA

SUMMARY OF EXPERIMENTAL CONDITIONS

A. COLD & HOT CALIBRATION

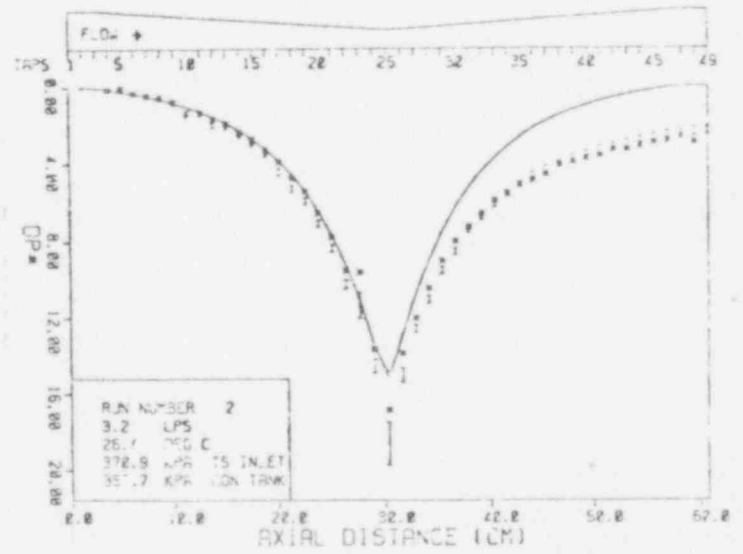
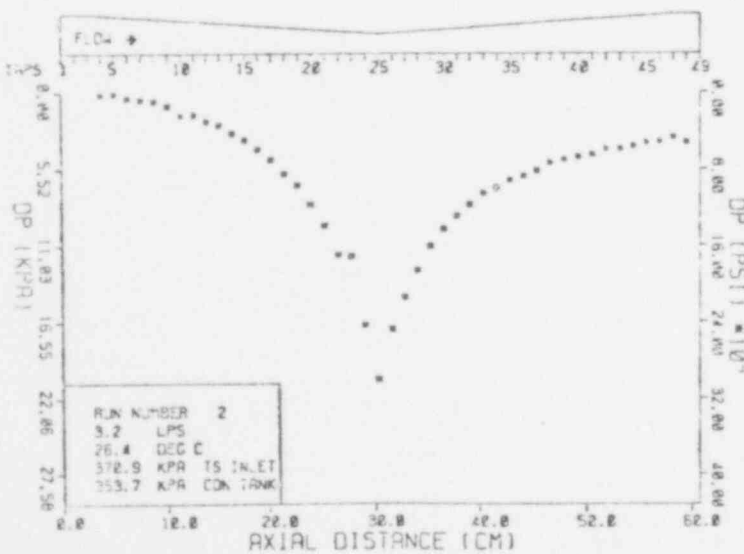
RUN	$P_{in}$ (kPa)	$T_{in}$ ( $^{\circ}$ C)	$G$ (Mg/m <sup>2</sup> s)	$P_{ct}$ (kPa)	$T_{ct}$ ( $^{\circ}$ C)
1	-----	-----	-----	---	-----
2	371	26.4	1.56	354	26.3
3	368	26.8	3.13	345	26.2
4	361	27.2	4.71	331	26.6
5	351	27.6	6.28	311	27.4
6	682	27.7	7.01	647	27.2
7	691	27.3	6.30	657	27.3
8	695	26.9	4.71	652	26.8
9	709	27.1	3.13	674	26.6
10	711	27.0	1.56	683	27.0
11	688	27.7	6.26	632	27.6
12	1033	29.2	7.01	973	29.1
13	1031	29.4	7.88	961	29.3
14	337	23.0	6.25	316	22.9
15	348	22.9	4.74	339	22.9
16	365	66.3	3.08	309	66.1
17	367	64.1	1.56	322	63.9
18	-----	-----	-----	---	-----
19	337	94.4	5.49	324	94.5
32	327	11.6	4.71	352	12.
33	315	11.9	6.29	326	11.9
34	336	12.3	3.15	369	12.3
36	293	69.1	3.08	308	68.9
62	692	148.4	2.33	646	148.4
70	213	54.0	3.35	201	48.6
71	211	54.4	3.34	203	48.8

# POOR ORIGINAL

## BML FLASHING FLOWS EXPERIMENT PRESSURE DROP DATA FROM TEST SECTION # 2

RUN NUMBER 2

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	T <sup>o</sup> INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-4	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	.17	.13
1-5	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	.19	.18
1-6	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	.40	.42
1-7	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	.52	.52
1-8	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	.63	.76
1-9	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	.73	.76
1-10	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	1.57	1.29
1-11	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	1.57	1.28
1-12	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	2.03	1.65
1-13	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	2.31	1.88
1-14	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	2.80	2.36
1-15	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	3.35	2.72
1-16	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	4.02	3.27
1-17	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	4.76	3.87
1-18	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	5.82	4.73
1-19	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	6.44	5.40
1-20	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	8.03	6.52
1-21	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	9.56	7.77
1-22	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	11.68	9.49
1-23	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	11.81	9.60
1-24	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	16.80	13.65
1-25	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	20.69	16.81
1-26	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	17.06	13.87
1-27	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	14.78	12.01
1-28	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	12.86	10.45
1-29	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	11.06	8.99
1-30	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	9.87	7.99
1-31	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	8.90	7.23
1-32	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	8.07	6.56
1-33	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	7.25	5.93
1-34	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	6.84	5.56
1-35	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	6.28	5.10
1-36	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	5.98	4.86
1-37	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	5.61	4.56
1-38	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	5.03	4.05
1-39	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	4.78	3.88
1-40	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	4.61	3.74
1-41	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	4.41	3.59
1-42	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	4.04	3.28
1-43	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	4.03	3.27
1-44	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	3.59	2.91
1-45	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	3.53	2.87
1-46	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	3.25	2.64
1-47	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	3.57	2.90
1-48	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	3.23	2.63
50-1	3.18	26.4	26.4	26.3	370.9	353.7	156.6	.914E+05	1.38	1.12



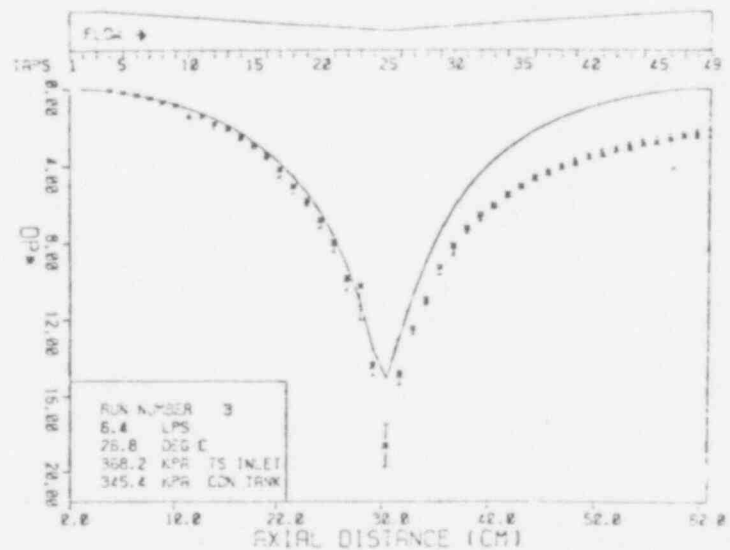
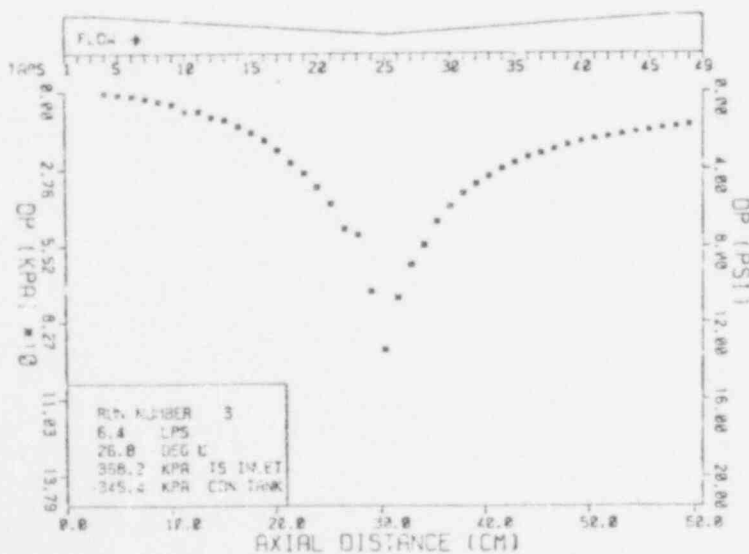
575 120

# POOR ORIGINAL

BNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER 3

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-4	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	.50	1.0
1-5	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	1.03	1.21
1-6	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	1.66	1.33
1-7	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	2.50	1.50
1-8	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	3.44	1.69
1-9	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	4.30	1.87
1-10	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	6.89	1.39
1-11	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	6.94	1.40
1-12	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	9.08	1.83
1-13	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	10.03	2.02
1-14	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	12.32	2.48
1-15	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	14.53	2.92
1-16	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	17.03	3.43
1-17	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	20.68	4.16
1-18	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	25.04	5.04
1-19	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	28.77	5.79
1-20	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	33.82	6.81
1-21	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	39.66	7.98
1-22	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	48.74	9.81
1-23	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	50.81	10.23
1-24	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	71.49	14.39
1-25	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	92.38	18.60
1-26	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	73.80	14.86
1-27	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	61.77	12.44
1-28	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	54.56	10.98
1-29	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	46.21	9.30
1-30	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	40.62	8.18
1-31	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	36.09	7.27
1-32	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	32.61	6.57
1-33	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	29.95	6.03
1-34	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	27.25	5.49
1-35	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	25.15	5.06
1-36	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	23.10	4.65
1-37	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	21.72	4.37
1-38	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	20.23	4.07
1-39	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	18.89	3.80
1-40	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	17.66	3.56
1-41	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	16.71	3.26
1-42	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	15.93	3.21
1-43	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	15.13	3.05
1-44	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	14.33	2.89
1-45	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	13.78	2.77
1-46	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	13.02	2.62
1-47	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	12.42	2.50
1-48	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	11.88	2.39
1-49	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	11.98	2.41
50-1	6.39	26.8	26.8	26.2	368.2	345.4	314.6	.185E+06	6.21	1.25

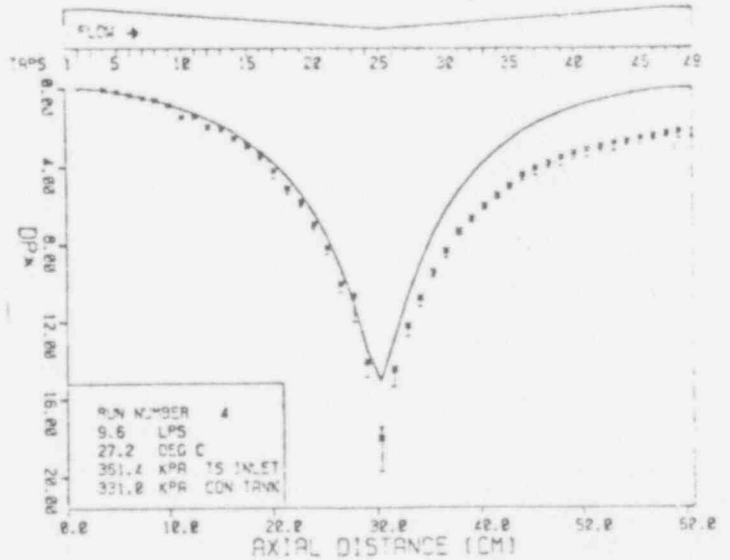
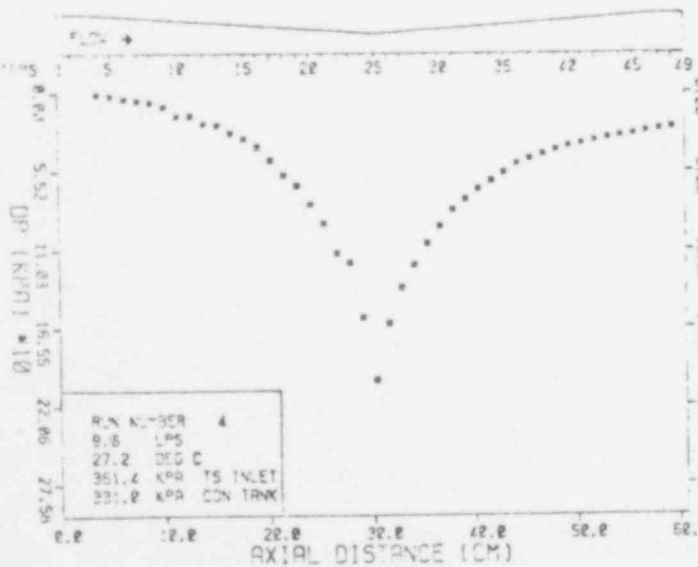


# POOR ORIGINAL

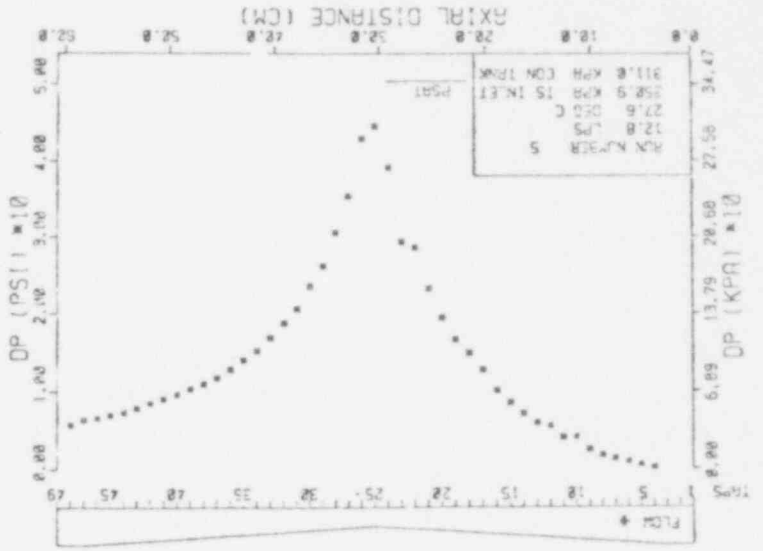
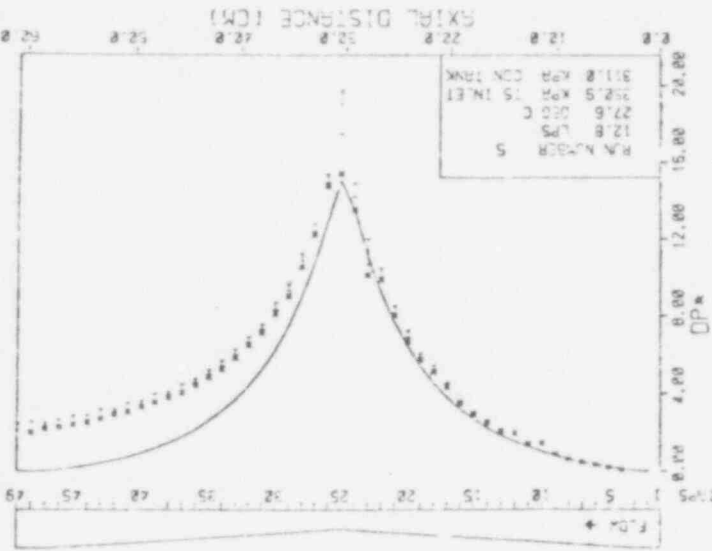
FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER 4

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)		PRESSURE (KPA)		VELOCITY CM/SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE MEASURED DIMENSIONLESS	
		FLOW METER	TS INLET	COND TANK	TS INLET			COND TANK	
1-4	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.261E+06	.99
1-5	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	2.34
1-6	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.291E+06	4.01
1-7	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	5.53
1-8	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	6.72
1-9	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	9.74
1-10	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	16.20
1-11	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	16.01
1-12	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	21.81
1-13	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	23.01
1-14	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	28.48
1-15	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	32.40
1-16	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	37.56
1-17	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	47.24
1-18	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	57.56
1-19	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	65.15
1-20	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	77.92
1-21	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	91.39
1-22	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	112.26
1-23	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	119.26
1-24	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	157.73
1-25	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	202.09
1-26	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	162.14
1-27	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	136.83
1-28	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	120.78
1-29	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	105.72
1-30	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	93.51
1-31	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	82.03
1-32	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	74.71
1-33	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	67.38
1-34	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	61.50
1-35	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	55.79
1-36	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	49.49
1-37	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	45.88
1-38	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	42.73
1-39	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	39.61
1-40	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	37.09
1-41	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	35.23
1-42	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	33.23
1-43	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	31.45
1-44	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	29.92
1-45	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	28.54
1-46	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	27.30
1-47	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	25.79
1-48	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	24.82
1-49	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	24.89
50-1	9.60	27.4	27.2	26.6	361.4	331.0	472.5	.281E+06	14.34







TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)	FLOW METER TS INLET COND TANK	PRESSURE (KPA)	IS INLET COND TANK	VELOCITY CM/SIC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE MEASURED DIMENSIONLESS
1-4	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	1.78
1-5	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	4.11
1-6	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	6.94
1-7	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	9.72
1-8	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	12.79
1-9	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	17.51
1-10	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	28.89
1-11	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	38.34
1-12	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	46.93
1-13	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	54.25
1-14	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	60.67
1-15	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	69.31
1-16	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	74.54
1-17	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	81.54
1-18	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	87.54
1-19	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	102.35
1-20	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	114.47
1-21	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	133.81
1-22	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	160.10
1-23	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	197.04
1-24	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	241.97
1-25	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	291.74
1-26	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	347.20
1-27	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	407.98
1-28	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	474.79
1-29	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	547.74
1-30	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	627.18
1-31	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	712.13
1-32	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	802.73
1-33	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	898.59
1-34	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	1000.17
1-35	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	1107.77
1-36	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	1221.77
1-37	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	1342.77
1-38	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	1470.77
1-39	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	1606.77
1-40	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	1750.77
1-41	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	1902.77
1-42	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	2062.77
1-43	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	2230.77
1-44	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	2407.77
1-45	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	2594.77
1-46	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	2791.77
1-47	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	2998.77
1-48	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	3215.77
1-49	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	3442.77
1-50	12.81	27.6	27.4	350.9	311.0	630.7	378E+06	3679.77

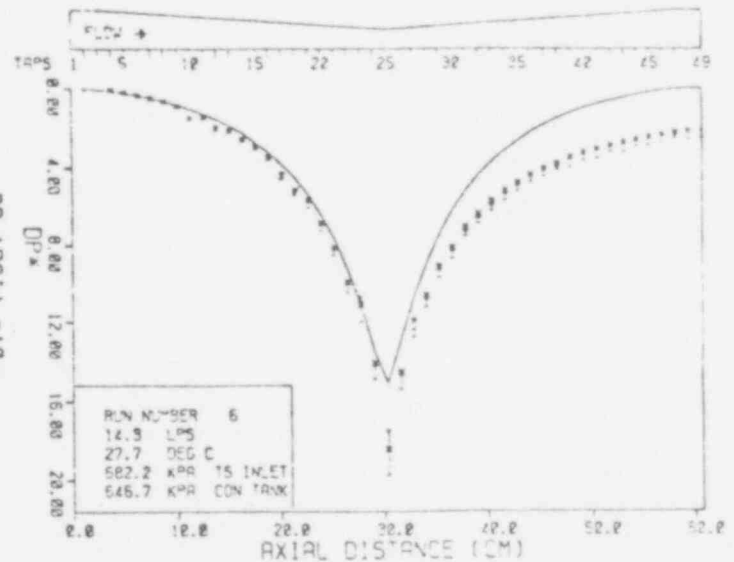
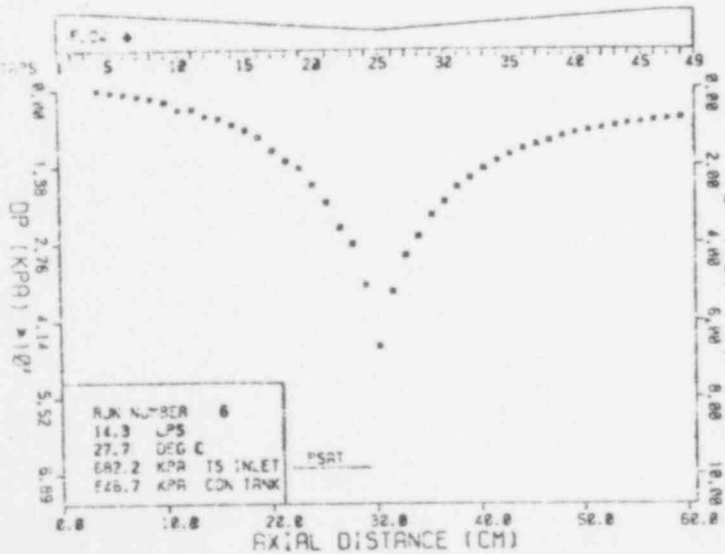
RUN NUMBER 5  
 TEST SECTION # 2  
 PRESSURE DROP DATA FROM  
 BLASTING FLOWS EXPERIMENT  
**POOR ORIGINAL**

# POOR ORIGINAL

## BNL FLASHING FLOWS EXPERIMENT PRESSURE DROP DATA FROM TEST SECTION # 2

RUN NUMBER 6

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-4	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	1.64	.07
1-5	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	4.95	.20
1-6	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	8.58	.35
1-7	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	12.02	.48
1-8	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	15.90	.64
1-9	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	21.70	.87
1-10	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	26.82	1.48
1-11	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	35.92	1.44
1-12	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	48.82	1.96
1-13	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	53.24	2.14
1-14	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	63.69	2.56
1-15	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	73.84	2.97
1-16	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	86.52	3.48
1-17	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	109.95	4.42
1-18	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	128.10	5.15
1-19	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	141.35	5.68
1-20	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	170.50	6.86
1-21	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	201.80	8.11
1-22	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	246.91	9.93
1-23	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	275.47	11.08
1-24	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	349.59	14.06
1-25	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	458.18	18.42
1-26	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	501.06	14.53
1-27	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	596.46	11.92
1-28	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	263.51	10.59
1-29	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	276.38	9.10
1-30	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	202.29	8.13
1-31	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	175.91	7.07
1-32	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	159.84	6.43
1-33	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	142.64	5.73
1-34	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	129.14	5.19
1-35	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	118.76	4.77
1-36	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	108.31	4.35
1-37	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	108.49	4.04
1-38	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	94.65	3.81
1-39	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	85.98	3.46
1-40	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	80.65	3.24
1-41	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	76.02	3.06
1-42	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	71.81	2.89
1-43	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	67.84	2.73
1-44	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	64.37	2.59
1-45	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	60.80	2.44
1-46	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	58.21	2.34
1-47	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	55.64	2.24
1-48	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	53.70	2.16
1-49	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	51.75	2.08
50-1	14.30	27.2	27.7	27.2	682.2	646.7	704.0	.423E+06	32.82	1.32

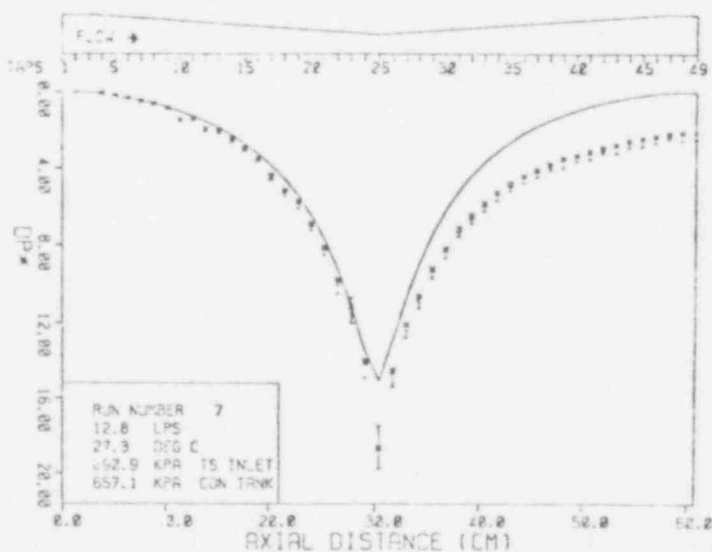
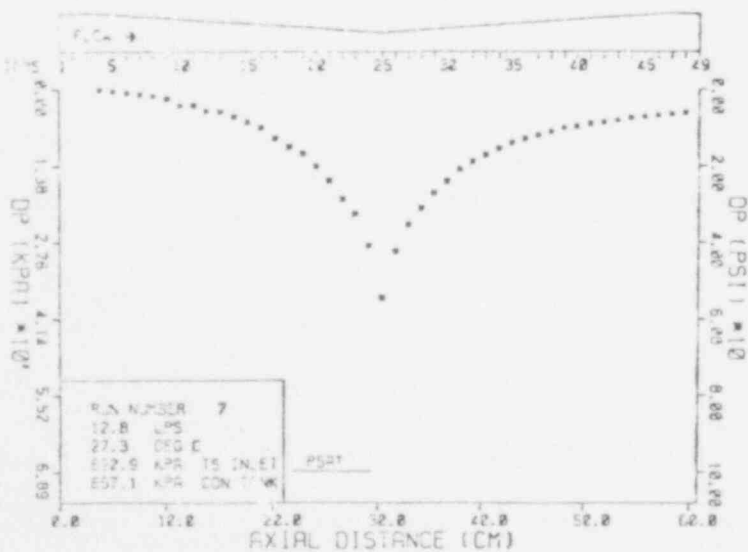


# POOR ORIGINAL

## BNL FLASHING FLOWS EXPERIMENT PRESSURE DROP DATA FROM TEST SECTION # 2

RUN NUMBER 7

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFF.ENTIAL PRESSURE MEASURED DIMENSIONLESS	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK				
1-4	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	1.64	.08
1-5	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	4.03	.20
1-6	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	6.73	.34
1-7	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	9.51	.47
1-8	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	12.65	.63
1-9	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	17.24	.86
1-10	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	24.15	1.45
1-11	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	28.38	1.41
1-12	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	39.03	1.94
1-13	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	41.54	2.07
1-14	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	49.55	2.47
1-15	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	59.34	2.95
1-16	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	69.79	3.45
1-17	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	88.19	4.39
1-18	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	103.42	5.15
1-19	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	114.81	5.72
1-20	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	137.99	6.87
1-21	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	163.14	8.12
1-22	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	196.18	9.76
1-23	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	232.74	11.09
1-24	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	281.12	14.08
1-25	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	374.48	18.65
1-26	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	291.14	14.50
1-27	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	242.41	12.07
1-28	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	212.86	10.60
1-29	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	185.31	9.23
1-30	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	164.65	8.20
1-31	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	143.18	7.13
1-32	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	129.68	6.46
1-33	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	117.20	5.88
1-34	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	100.20	5.29
1-35	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	96.36	4.80
1-36	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	88.47	4.41
1-37	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	82.03	3.99
1-38	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	76.13	3.79
1-39	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	69.50	3.48
1-40	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	66.58	3.32
1-41	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	62.10	3.09
1-42	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	58.96	2.94
1-43	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	55.69	2.77
1-44	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	51.28	2.55
1-45	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	49.05	2.44
1-46	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	46.80	2.33
1-47	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	44.55	2.22
1-48	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	43.02	2.14
1-49	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	42.61	2.12
50-1	12.85	27.3	27.3	27.3	690.9	657.1	632.5	.377E+06	25.51	1.27

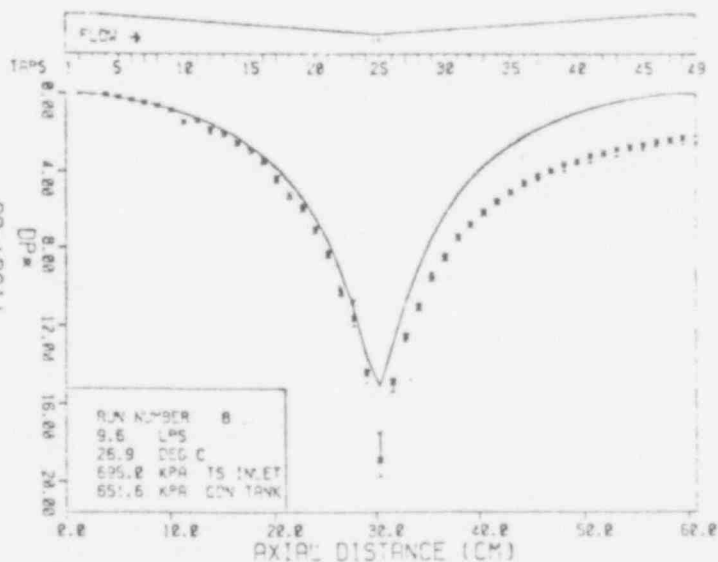
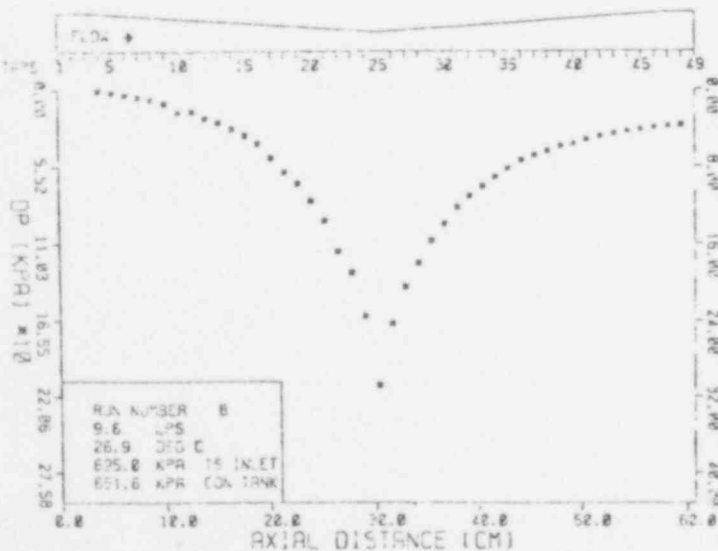


# POOR ORIGINAL

BNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER B

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C) FLOW METER TS INLET COND TANK	PRESSURE (KPA) TS INLET COND TANK	VELOCITY CM/SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE MEASURED DIMENSIONLESS
1-4	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	1.95
1-5	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	2.20
1-6	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	3.91
1-7	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	5.50
1-8	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	7.15
1-9	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	9.72
1-10	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	12.34
1-11	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	15.80
1-12	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	20.71
1-13	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	23.51
1-14	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	28.38
1-15	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	32.90
1-16	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	38.71
1-17	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	48.88
1-18	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	59.14
1-19	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	67.32
1-20	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	79.79
1-21	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	93.80
1-22	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	115.49
1-23	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	130.31
1-24	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	161.75
1-25	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	212.18
1-26	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	167.09
1-27	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	140.81
1-28	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	124.00
1-29	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	109.12
1-30	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	96.27
1-31	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	84.48
1-32	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	76.44
1-33	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	69.41
1-34	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	63.00
1-35	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	56.94
1-36	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	50.76
1-37	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	47.12
1-38	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	44.18
1-39	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	40.57
1-40	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	38.87
1-41	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	35.82
1-42	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	33.76
1-43	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	31.83
1-44	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	30.09
1-45	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	28.81
1-46	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	27.42
1-47	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	26.11
1-48	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	25.71
1-49	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	24.99
50-1	9.61	26.9 26.9 26.8	695.0 651.6	473.1	2.79E+06	14.48

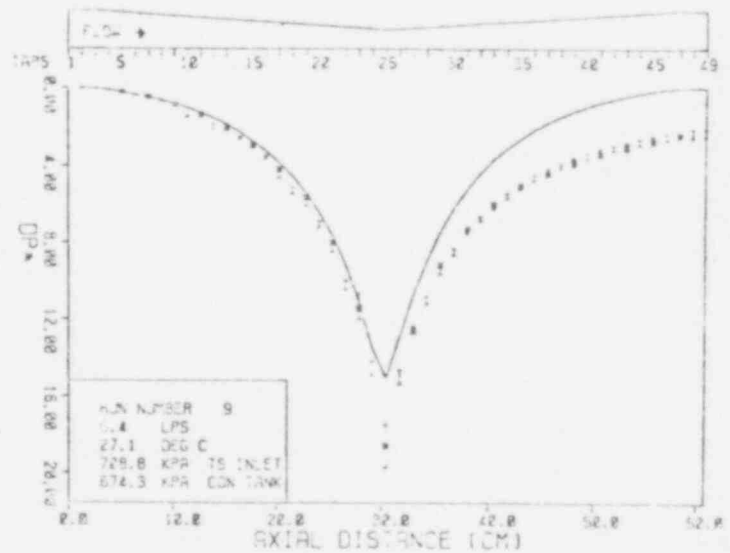
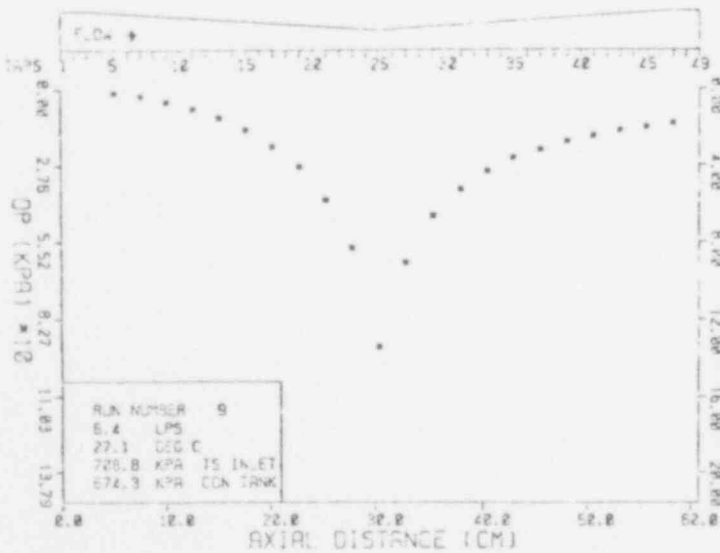


# POOR ORIGINAL

BNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER 9

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-5	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	1.06	.21
1-7	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	2.28	.46
1-9	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	4.37	.88
1-11	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	6.87	1.38
1-13	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	10.09	2.03
1-15	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	14.47	2.91
1-17	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	20.69	4.16
1-19	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	27.91	5.61
1-21	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	39.77	8.01
1-23	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	57.05	11.44
1-25	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	92.40	18.59
1-27	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	62.66	12.60
1-29	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	45.77	9.21
1-31	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	36.20	7.28
1-33	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	29.71	5.94
1-35	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	24.88	5.00
1-37	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	21.93	4.41
1-39	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	18.84	3.79
1-41	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	16.76	3.37
1-43	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	14.91	3.00
1-45	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	13.67	2.75
1-47	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	12.29	2.47
1-49	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	12.10	2.43
50-1	6.39	27.4	27.1	26.6	708.8	674.3	314.7	.187E+06	6.21	1.25

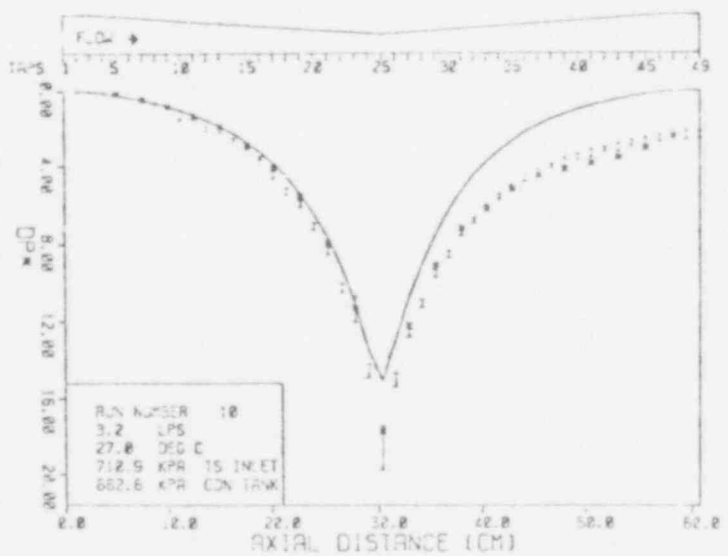
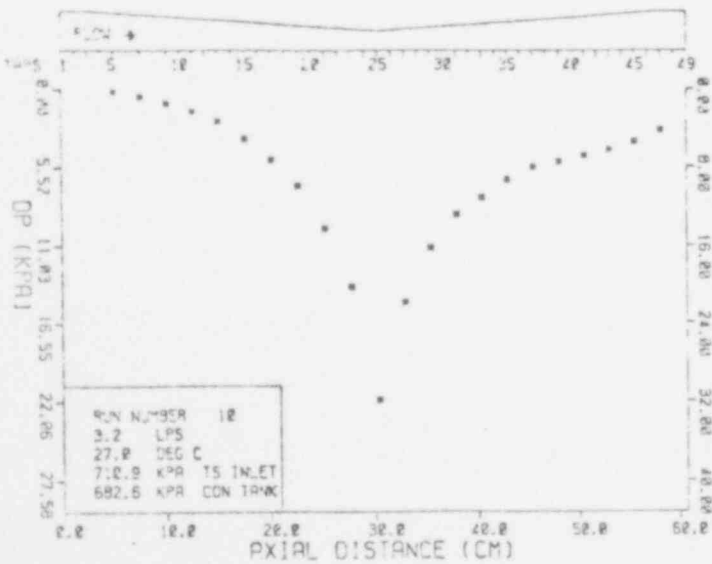


# POOR ORIGINAL

BNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER 10

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-5	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	.18	.15
1-7	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	.52	.42
1-9	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	1.01	.82
1-11	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	1.63	1.29
1-13	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	2.32	1.88
1-15	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	3.54	2.87
1-17	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	5.00	4.05
1-19	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	6.80	5.50
1-21	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	9.78	7.92
1-23	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	13.92	11.27
1-25	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	21.91	17.73
1-27	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	35.04	28.17
1-29	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	51.20	40.06
1-31	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	71.65	56.19
1-33	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	97.39	77.17
1-35	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	130.52	104.47
1-37	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	173.15	140.17
1-39	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	227.41	180.81
1-41	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	295.28	237.50
1-43	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	378.76	302.15
1-45	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	479.95	377.29
1-47	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	599.87	466.57
1-49	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	739.54	573.12
50-1	3.19	27.3	27.0	27.0	710.9	682.6	156.9	.929E+05	899.96	699.12

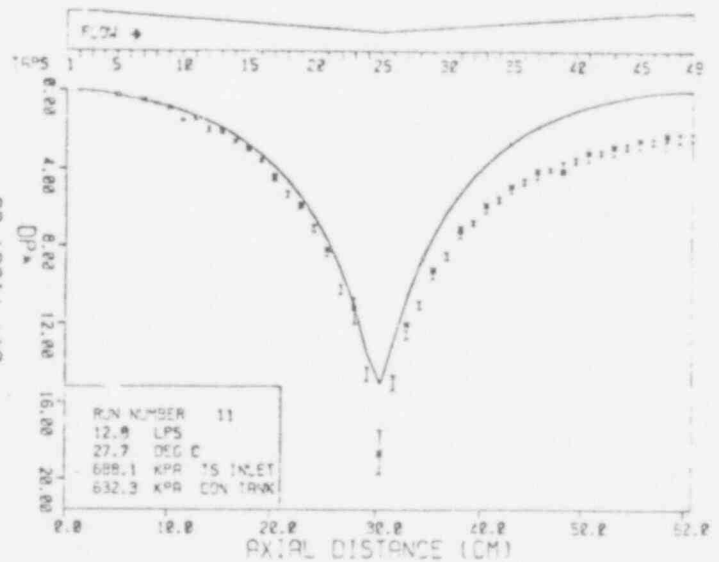
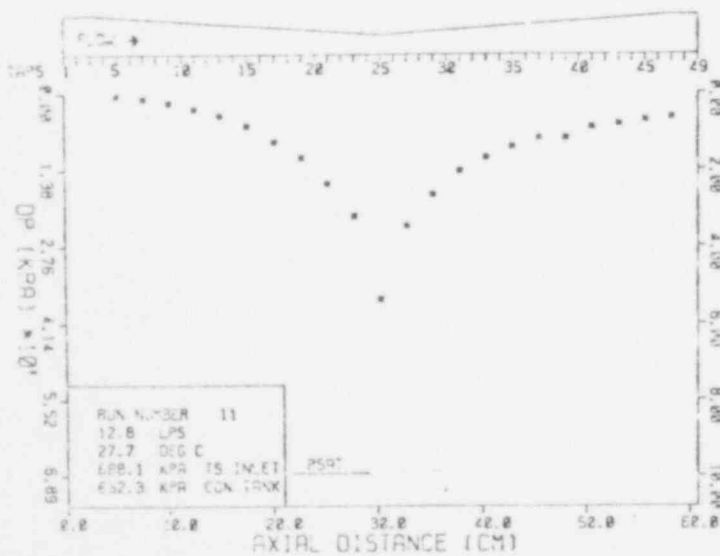


BNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER 11

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-5	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	4.32	.22
1-7	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	9.67	.49
1-9	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	17.02	.86
1-11	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	27.73	1.40
1-13	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	40.31	2.03
1-15	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	58.68	2.96
1-17	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	87.67	4.42
1-19	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	115.71	5.83
1-21	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	161.78	8.15
1-23	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	221.48	11.16
1-25	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	270.54	14.67
1-27	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	239.39	12.46
1-29	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	182.85	9.21
1-31	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	140.25	7.07
1-33	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	115.01	5.85
1-35	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	96.33	4.85
1-37	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	80.62	4.06
1-39	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	80.89	4.08
1-41	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	61.36	3.09
1-43	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	55.17	2.78
1-45	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	48.27	2.44
1-47	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	43.69	2.20
1-49	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	41.40	2.09
50-1	12.77	27.6	27.7	27.6	688.1	632.3	628.8	.378E+06	25.51	1.29

**POOR ORIGINAL**

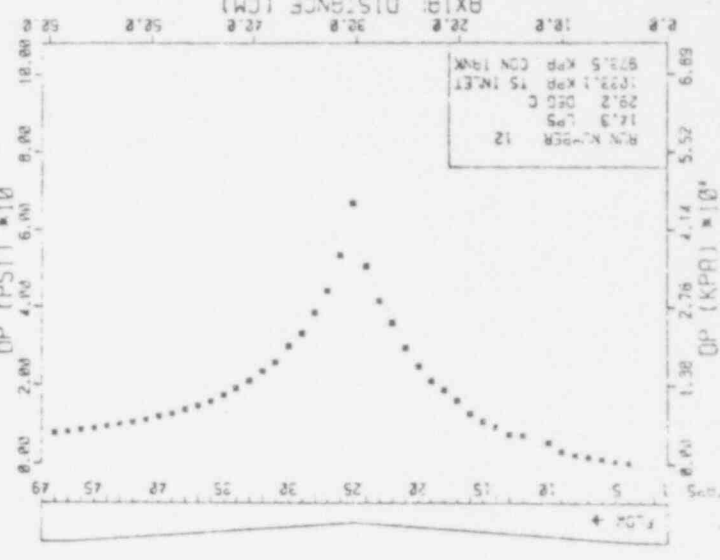
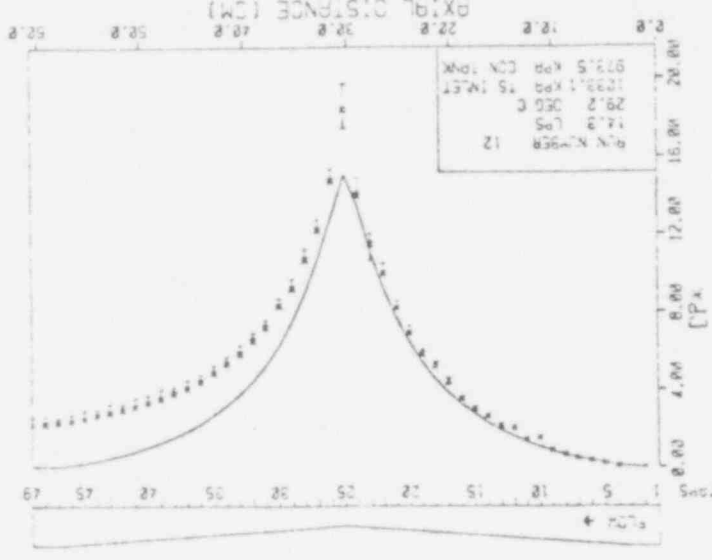


POOR ORIGINAL

BML FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER 12

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C) FLOW METER TS INLET COND TANK	PRESSURE (KPA) TS INLET COND TANK	VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE MEASURED DIMENSIONLESS
1-4	14.30	29.1	1033.1	704.3	439E+06	2.15
1-5	14.30	29.1	1033.1	704.3	439E+06	5.07
1-6	14.30	29.1	1033.1	704.3	439E+06	8.71
1-7	14.30	29.1	1033.1	704.3	439E+06	12.29
1-8	14.30	29.1	1033.1	704.3	439E+06	16.14
1-9	14.30	29.1	1033.1	704.3	439E+06	21.68
1-10	14.30	29.1	1033.1	704.3	439E+06	29.23
1-12	14.30	29.1	1033.1	704.3	439E+06	49.70
1-13	14.30	29.1	1033.1	704.3	439E+06	61.87
1-14	14.30	29.1	1033.1	704.3	439E+06	64.55
1-15	14.30	29.1	1033.1	704.3	439E+06	74.00
1-16	14.30	29.1	1033.1	704.3	439E+06	87.46
1-17	14.30	29.1	1033.1	704.3	439E+06	110.61
1-18	14.30	29.1	1033.1	704.3	439E+06	139.71
1-19	14.30	29.1	1033.1	704.3	439E+06	184.55
1-20	14.30	29.1	1033.1	704.3	439E+06	243.39
1-21	14.30	29.1	1033.1	704.3	439E+06	327.77
1-23	14.30	29.1	1033.1	704.3	439E+06	585.73
1-25	14.30	29.1	1033.1	704.3	439E+06	967.44
1-27	14.30	29.1	1033.1	704.3	439E+06	1413.72
1-28	14.30	29.1	1033.1	704.3	439E+06	2057.44
1-29	14.30	29.1	1033.1	704.3	439E+06	2925.44
1-30	14.30	29.1	1033.1	704.3	439E+06	4076.72
1-31	14.30	29.1	1033.1	704.3	439E+06	5706.72
1-32	14.30	29.1	1033.1	704.3	439E+06	7911.99
1-33	14.30	29.1	1033.1	704.3	439E+06	10911.81
1-34	14.30	29.1	1033.1	704.3	439E+06	15071.44
1-35	14.30	29.1	1033.1	704.3	439E+06	21111.81
1-36	14.30	29.1	1033.1	704.3	439E+06	29211.81
1-37	14.30	29.1	1033.1	704.3	439E+06	40111.81
1-38	14.30	29.1	1033.1	704.3	439E+06	54911.81
1-40	14.30	29.1	1033.1	704.3	439E+06	75911.81
1-41	14.30	29.1	1033.1	704.3	439E+06	105411.81
1-42	14.30	29.1	1033.1	704.3	439E+06	145411.81
1-43	14.30	29.1	1033.1	704.3	439E+06	199411.81
1-44	14.30	29.1	1033.1	704.3	439E+06	274411.81
1-45	14.30	29.1	1033.1	704.3	439E+06	378411.81
1-46	14.30	29.1	1033.1	704.3	439E+06	519411.81
1-47	14.30	29.1	1033.1	704.3	439E+06	708411.81
1-48	14.30	29.1	1033.1	704.3	439E+06	961411.81
1-49	14.30	29.1	1033.1	704.3	439E+06	1308411.81
50-1	14.30	29.1	1033.1	704.3	439E+06	17708



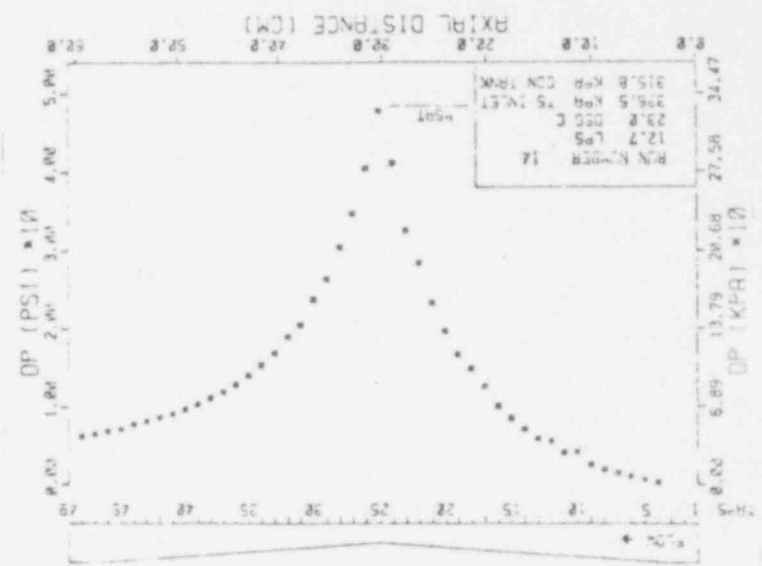
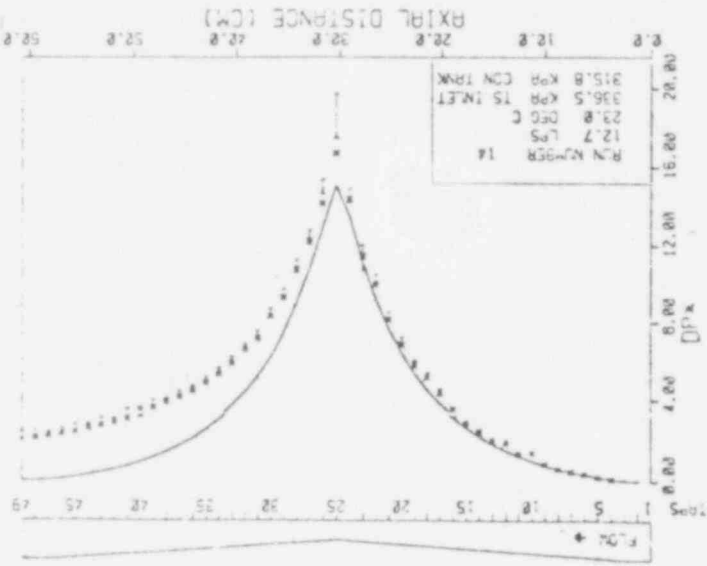
575 130





575 132

-100-



TAPS	TEMPERATURES (DEG C)	FLOW METER TS INLET COND TANK	TS INLET COND TANK	PRESSURE (KPA)	VELOCITY	REYNOLDS	DIFFERENTIAL PRESSURES
50-1	22.4	23.4	22.9	336.5	315.8	626.3	25.51
1-49	23.0	23.0	22.9	336.5	315.8	626.3	42.49
1-48	23.0	23.0	22.9	336.5	315.8	626.3	42.87
1-47	23.0	23.0	22.9	336.5	315.8	626.3	44.51
1-46	23.0	23.0	22.9	336.5	315.8	626.3	46.30
1-45	23.0	23.0	22.9	336.5	315.8	626.3	48.75
1-44	23.0	23.0	22.9	336.5	315.8	626.3	53.10
1-43	23.0	23.0	22.9	336.5	315.8	626.3	55.82
1-42	23.0	23.0	22.9	336.5	315.8	626.3	59.01
1-41	23.0	23.0	22.9	336.5	315.8	626.3	62.52
1-40	23.0	23.0	22.9	336.5	315.8	626.3	66.62
1-39	23.0	23.0	22.9	336.5	315.8	626.3	71.09
1-38	23.0	23.0	22.9	336.5	315.8	626.3	76.53
1-37	23.0	23.0	22.9	336.5	315.8	626.3	81.60
1-36	23.0	23.0	22.9	336.5	315.8	626.3	88.43
1-35	23.0	23.0	22.9	336.5	315.8	626.3	96.37
1-34	23.0	23.0	22.9	336.5	315.8	626.3	105.27
1-33	23.0	23.0	22.9	336.5	315.8	626.3	116.53
1-32	23.0	23.0	22.9	336.5	315.8	626.3	130.50
1-31	23.0	23.0	22.9	336.5	315.8	626.3	148.31
1-30	23.0	23.0	22.9	336.5	315.8	626.3	168.11
1-29	23.0	23.0	22.9	336.5	315.8	626.3	182.33
1-28	23.0	23.0	22.9	336.5	315.8	626.3	210.31
1-27	23.0	23.0	22.9	336.5	315.8	626.3	239.41
1-26	23.0	23.0	22.9	336.5	315.8	626.3	279.01
1-25	23.0	23.0	22.9	336.5	315.8	626.3	329.15
1-24	23.0	23.0	22.9	336.5	315.8	626.3	389.22
1-23	23.0	23.0	22.9	336.5	315.8	626.3	460.12
1-22	23.0	23.0	22.9	336.5	315.8	626.3	543.14
1-21	23.0	23.0	22.9	336.5	315.8	626.3	639.35
1-20	23.0	23.0	22.9	336.5	315.8	626.3	750.24
1-19	23.0	23.0	22.9	336.5	315.8	626.3	878.99
1-18	23.0	23.0	22.9	336.5	315.8	626.3	1029.60
1-17	23.0	23.0	22.9	336.5	315.8	626.3	1207.00
1-16	23.0	23.0	22.9	336.5	315.8	626.3	1416.54
1-15	23.0	23.0	22.9	336.5	315.8	626.3	1664.27
1-14	23.0	23.0	22.9	336.5	315.8	626.3	1957.22
1-13	23.0	23.0	22.9	336.5	315.8	626.3	2302.27
1-12	23.0	23.0	22.9	336.5	315.8	626.3	2707.27
1-11	23.0	23.0	22.9	336.5	315.8	626.3	3182.27
1-10	23.0	23.0	22.9	336.5	315.8	626.3	3737.27
1-9	23.0	23.0	22.9	336.5	315.8	626.3	4382.27
1-8	23.0	23.0	22.9	336.5	315.8	626.3	5127.27
1-7	23.0	23.0	22.9	336.5	315.8	626.3	5982.27
1-6	23.0	23.0	22.9	336.5	315.8	626.3	6957.27
1-5	23.0	23.0	22.9	336.5	315.8	626.3	8072.27
1-4	23.0	23.0	22.9	336.5	315.8	626.3	9347.27

BNL FLASHING FLOWS EXPERIMENT

TEST SECTION # 2

RUN NUMBER 14

**POOR ORIGINAL**





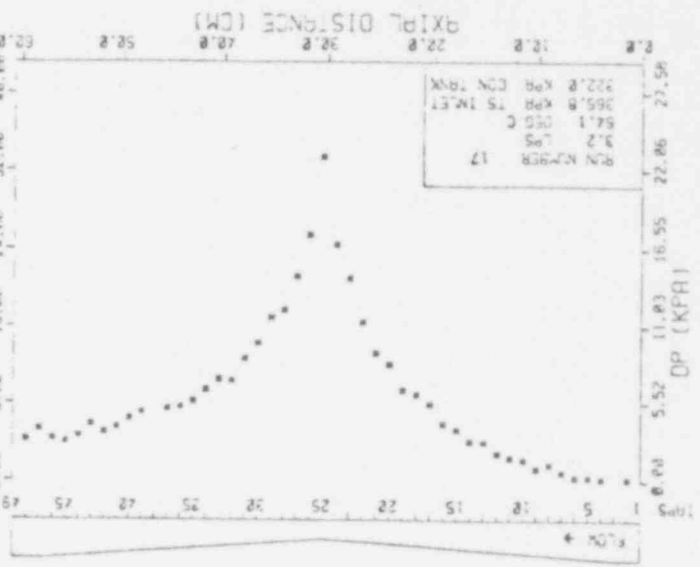
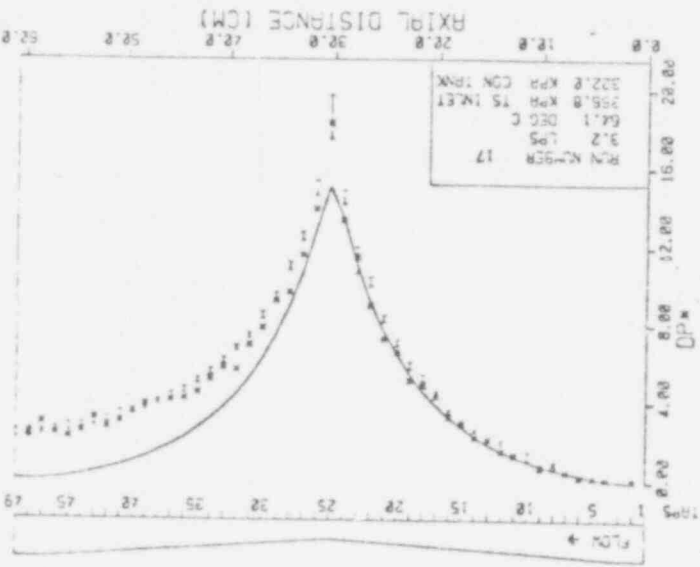
POOR ORIGINAL

BNL FLASHING FLOWS EXPERIMENT

TEST SECTION # 2

RUN NUMBER 17

TAPS	TEMPERATURES (DEG C)	PRESSURE (KPA)	VELOCITY	REYNOLDS	DIFFERENTIAL PRESSURE
	TS INLET COND TANK	TS INLET COND TANK	CM SIDC	MUMBER	MEASURED DIMENSIONLESS
1-2	60.5	366.8	159.2	1798.06	1.14
1-4	60.5	366.8	159.2	1798.06	1.18
1-6	60.5	366.8	159.2	1798.06	1.23
1-8	60.5	366.8	159.2	1798.06	1.27
1-10	60.5	366.8	159.2	1798.06	1.31
1-11	60.5	366.8	159.2	1798.06	1.35
1-12	60.5	366.8	159.2	1798.06	1.39
1-13	60.5	366.8	159.2	1798.06	1.43
1-14	60.5	366.8	159.2	1798.06	1.47
1-15	60.5	366.8	159.2	1798.06	1.51
1-16	60.5	366.8	159.2	1798.06	1.55
1-17	60.5	366.8	159.2	1798.06	1.59
1-18	60.5	366.8	159.2	1798.06	1.63
1-19	60.5	366.8	159.2	1798.06	1.67
1-20	60.5	366.8	159.2	1798.06	1.71
1-21	60.5	366.8	159.2	1798.06	1.75
1-22	60.5	366.8	159.2	1798.06	1.79
1-23	60.5	366.8	159.2	1798.06	1.83
1-24	60.5	366.8	159.2	1798.06	1.87
1-25	60.5	366.8	159.2	1798.06	1.91
1-26	60.5	366.8	159.2	1798.06	1.95
1-27	60.5	366.8	159.2	1798.06	1.99
1-28	60.5	366.8	159.2	1798.06	2.03
1-29	60.5	366.8	159.2	1798.06	2.07
1-30	60.5	366.8	159.2	1798.06	2.11
1-31	60.5	366.8	159.2	1798.06	2.15
1-32	60.5	366.8	159.2	1798.06	2.19
1-33	60.5	366.8	159.2	1798.06	2.23
1-34	60.5	366.8	159.2	1798.06	2.27
1-35	60.5	366.8	159.2	1798.06	2.31
1-36	60.5	366.8	159.2	1798.06	2.35
1-37	60.5	366.8	159.2	1798.06	2.39
1-38	60.5	366.8	159.2	1798.06	2.43
1-39	60.5	366.8	159.2	1798.06	2.47
1-40	60.5	366.8	159.2	1798.06	2.51
1-41	60.5	366.8	159.2	1798.06	2.55
1-42	60.5	366.8	159.2	1798.06	2.59
1-43	60.5	366.8	159.2	1798.06	2.63
1-44	60.5	366.8	159.2	1798.06	2.67
1-45	60.5	366.8	159.2	1798.06	2.71
1-46	60.5	366.8	159.2	1798.06	2.75
1-47	60.5	366.8	159.2	1798.06	2.79
1-48	60.5	366.8	159.2	1798.06	2.83
1-49	60.5	366.8	159.2	1798.06	2.87
1-50	60.5	366.8	159.2	1798.06	2.91

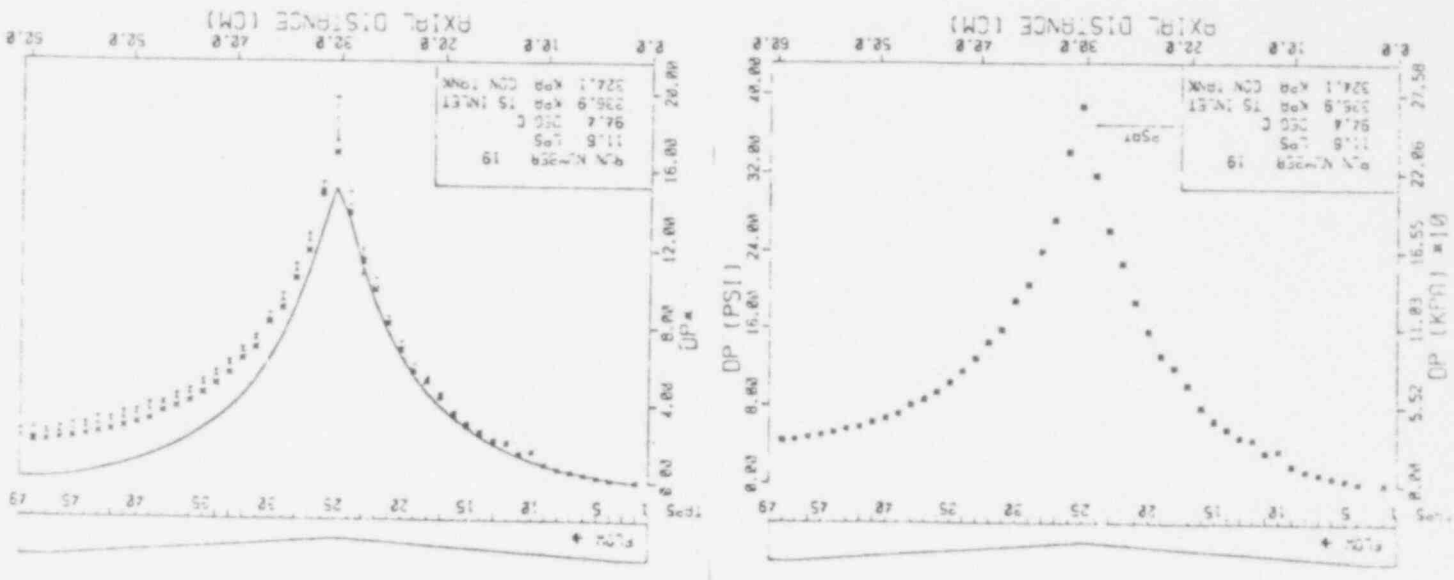


POON ORIGINAL

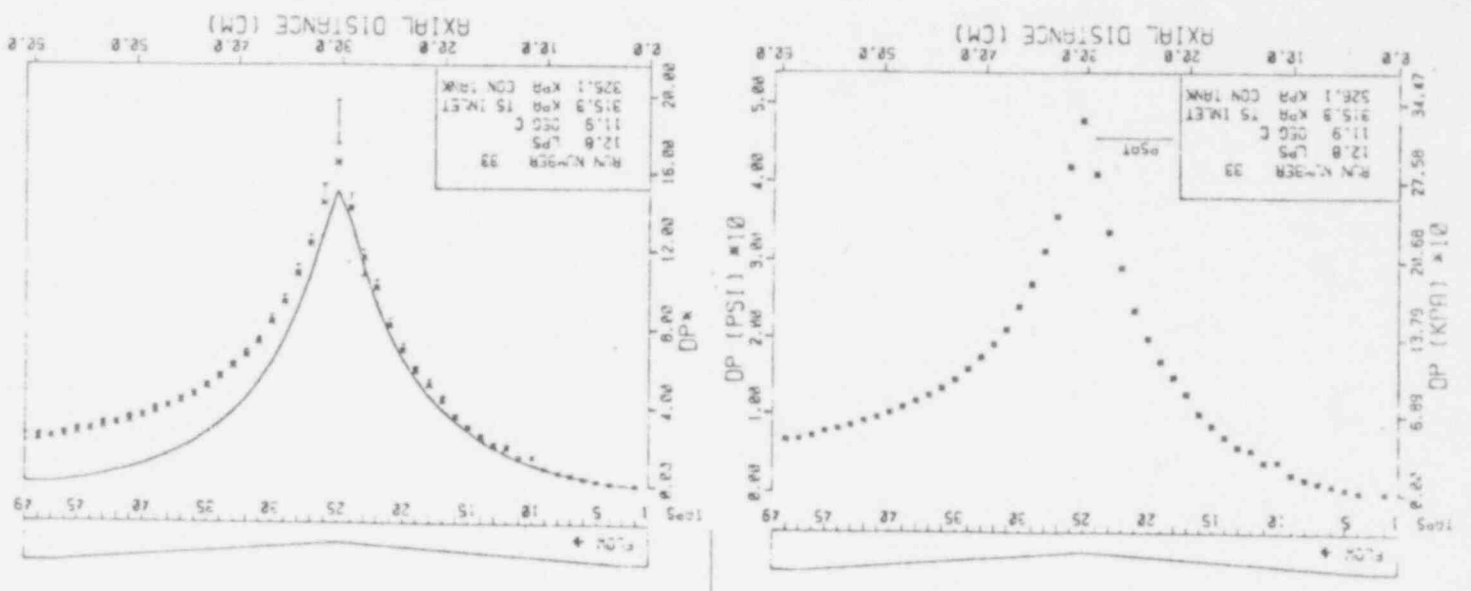
BNL FLASHING PLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER 19

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DBG C) FLOW METER TS INLET COND TANK	PRESSURE (KPA) TS INLET COND TANK	VELOCITY (M/S)	WETTED SURFACE AREA (CM <sup>2</sup> )	DIFFERENTIAL PRESSURE MEASURED DIMENSIONLESS
1-2	11.60	94.6	336.9	571.0	923E+06	1.01
1-5	11.60	94.6	336.9	571.0	923E+06	1.09
1-6	11.60	94.6	336.9	571.0	923E+06	1.20
1-7	11.60	94.6	336.9	571.0	923E+06	1.34
1-8	11.60	94.6	336.9	571.0	923E+06	1.47
1-9	11.60	94.6	336.9	571.0	923E+06	1.62
1-10	11.60	94.6	336.9	571.0	923E+06	1.78
1-11	11.60	94.6	336.9	571.0	923E+06	1.95
1-12	11.60	94.6	336.9	571.0	923E+06	2.13
1-13	11.60	94.6	336.9	571.0	923E+06	2.30
1-14	11.60	94.6	336.9	571.0	923E+06	2.48
1-15	11.60	94.6	336.9	571.0	923E+06	2.66
1-16	11.60	94.6	336.9	571.0	923E+06	2.84
1-17	11.60	94.6	336.9	571.0	923E+06	3.03
1-18	11.60	94.6	336.9	571.0	923E+06	3.21
1-19	11.60	94.6	336.9	571.0	923E+06	3.40
1-20	11.60	94.6	336.9	571.0	923E+06	3.58
1-21	11.60	94.6	336.9	571.0	923E+06	3.78
1-22	11.60	94.6	336.9	571.0	923E+06	3.98
1-23	11.60	94.6	336.9	571.0	923E+06	4.18
1-24	11.60	94.6	336.9	571.0	923E+06	4.38
1-25	11.60	94.6	336.9	571.0	923E+06	4.58
1-26	11.60	94.6	336.9	571.0	923E+06	4.78
1-27	11.60	94.6	336.9	571.0	923E+06	4.98
1-28	11.60	94.6	336.9	571.0	923E+06	5.18
1-29	11.60	94.6	336.9	571.0	923E+06	5.38
1-30	11.60	94.6	336.9	571.0	923E+06	5.58
1-31	11.60	94.6	336.9	571.0	923E+06	5.78
1-32	11.60	94.6	336.9	571.0	923E+06	5.98
1-33	11.60	94.6	336.9	571.0	923E+06	6.18
1-34	11.60	94.6	336.9	571.0	923E+06	6.38
1-35	11.60	94.6	336.9	571.0	923E+06	6.58
1-36	11.60	94.6	336.9	571.0	923E+06	6.78
1-37	11.60	94.6	336.9	571.0	923E+06	6.98
1-38	11.60	94.6	336.9	571.0	923E+06	7.18
1-39	11.60	94.6	336.9	571.0	923E+06	7.38
1-40	11.60	94.6	336.9	571.0	923E+06	7.58
1-41	11.60	94.6	336.9	571.0	923E+06	7.78
1-42	11.60	94.6	336.9	571.0	923E+06	7.98
1-43	11.60	94.6	336.9	571.0	923E+06	8.18
1-44	11.60	94.6	336.9	571.0	923E+06	8.38
1-45	11.60	94.6	336.9	571.0	923E+06	8.58
1-46	11.60	94.6	336.9	571.0	923E+06	8.78
1-47	11.60	94.6	336.9	571.0	923E+06	8.98
1-48	11.60	94.6	336.9	571.0	923E+06	9.18
1-49	11.60	94.6	336.9	571.0	923E+06	9.38
50-1	11.60	94.6	336.9	571.0	923E+06	9.58







TAPS	TEMPERATURES (DEG C)	TEMPERATURES (DEG F)	TS INLET COND TANK	TS INLET COND TANK	VELOCITY	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	MEASURED DIMENSIONS
1-2	11.9	53.4	326.1	326.1	629.7	2578	2.01	1.05
1-5	11.9	53.4	326.1	326.1	629.7	2578	4.78	2.2
1-6	11.9	53.4	326.1	326.1	629.7	2578	6.95	3.5
1-7	11.9	53.4	326.1	326.1	629.7	2578	9.94	5.0
1-8	11.9	53.4	326.1	326.1	629.7	2578	12.89	6.5
1-8	11.9	53.4	326.1	326.1	629.7	2578	17.35	8.7
1-11	11.9	53.4	326.1	326.1	629.7	2578	27.87	14.2
1-12	11.9	53.4	326.1	326.1	629.7	2578	38.28	19.7
1-13	11.9	53.4	326.1	326.1	629.7	2578	49.91	26.5
1-14	11.9	53.4	326.1	326.1	629.7	2578	62.77	33.0
1-15	11.9	53.4	326.1	326.1	629.7	2578	76.91	40.5
1-16	11.9	53.4	326.1	326.1	629.7	2578	92.27	49.5
1-17	11.9	53.4	326.1	326.1	629.7	2578	109.17	60.0
1-18	11.9	53.4	326.1	326.1	629.7	2578	127.57	72.5
1-19	11.9	53.4	326.1	326.1	629.7	2578	148.88	87.5
1-20	11.9	53.4	326.1	326.1	629.7	2578	172.30	105.5
1-21	11.9	53.4	326.1	326.1	629.7	2578	200.77	126.5
1-22	11.9	53.4	326.1	326.1	629.7	2578	231.99	150.5
1-23	11.9	53.4	326.1	326.1	629.7	2578	267.31	177.5
1-24	11.9	53.4	326.1	326.1	629.7	2578	307.27	207.5
1-25	11.9	53.4	326.1	326.1	629.7	2578	352.49	240.5
1-26	11.9	53.4	326.1	326.1	629.7	2578	403.51	276.5
1-27	11.9	53.4	326.1	326.1	629.7	2578	460.96	315.5
1-28	11.9	53.4	326.1	326.1	629.7	2578	525.29	357.5
1-29	11.9	53.4	326.1	326.1	629.7	2578	597.19	402.5
1-30	11.9	53.4	326.1	326.1	629.7	2578	677.27	450.5
1-31	11.9	53.4	326.1	326.1	629.7	2578	766.17	501.5
1-32	11.9	53.4	326.1	326.1	629.7	2578	864.53	556.5
1-33	11.9	53.4	326.1	326.1	629.7	2578	972.97	615.5
1-34	11.9	53.4	326.1	326.1	629.7	2578	1091.17	678.5
1-35	11.9	53.4	326.1	326.1	629.7	2578	1219.77	745.5
1-36	11.9	53.4	326.1	326.1	629.7	2578	1358.47	816.5
1-37	11.9	53.4	326.1	326.1	629.7	2578	1506.96	891.5
1-38	11.9	53.4	326.1	326.1	629.7	2578	1665.06	970.5
1-39	11.9	53.4	326.1	326.1	629.7	2578	1833.56	1053.5
1-40	11.9	53.4	326.1	326.1	629.7	2578	2012.26	1150.5
1-41	11.9	53.4	326.1	326.1	629.7	2578	2201.96	1261.5
1-42	11.9	53.4	326.1	326.1	629.7	2578	2402.46	1386.5
1-43	11.9	53.4	326.1	326.1	629.7	2578	2613.56	1525.5
1-44	11.9	53.4	326.1	326.1	629.7	2578	2835.06	1678.5
1-45	11.9	53.4	326.1	326.1	629.7	2578	3066.76	1845.5
1-46	11.9	53.4	326.1	326.1	629.7	2578	3308.46	2026.5
1-47	11.9	53.4	326.1	326.1	629.7	2578	3560.06	2221.5
1-48	11.9	53.4	326.1	326.1	629.7	2578	3821.46	2430.5
1-49	11.9	53.4	326.1	326.1	629.7	2578	4092.46	2653.5
50-1	11.9	53.4	326.1	326.1	629.7	2578	4373.76	2890.5

BNL PLANNING DIVISION EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2  
**POOR ORIGINAL**

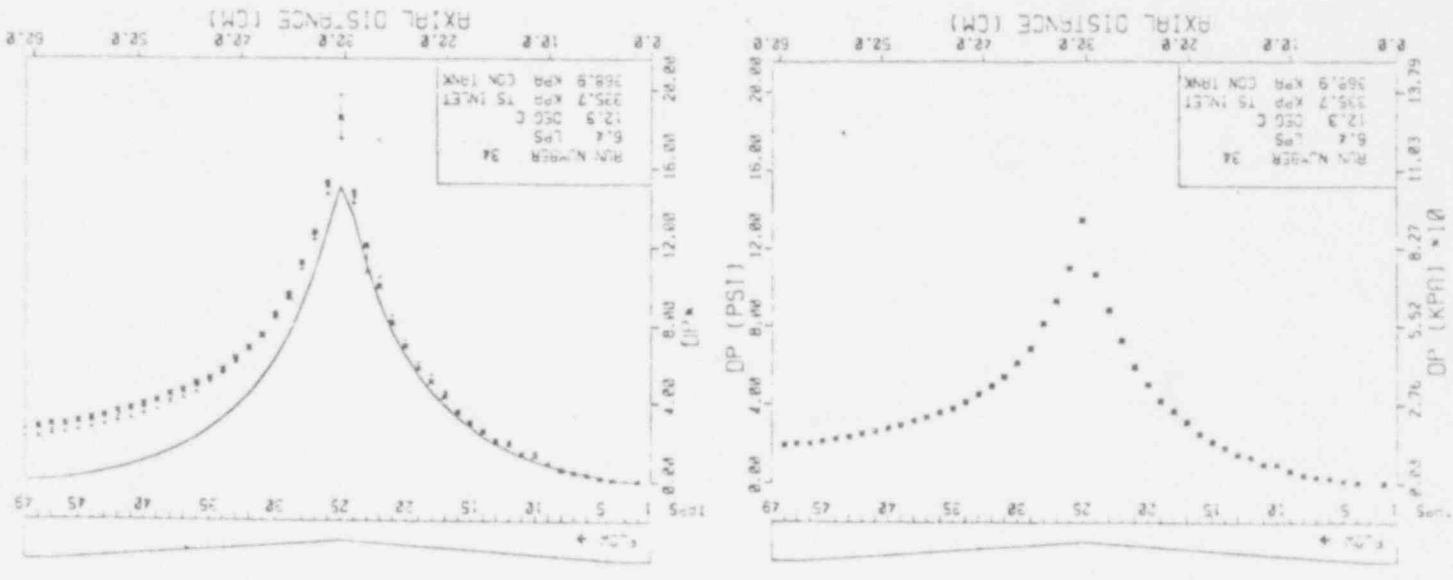


**POOR ORIGINAL**

BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 34

TAPS	LOOP FLOW LIT/SEC	TEMPERATURES (DEG C) FLOW METER TS INLET COND TANK	PRESSURE (KPA) COND TANK TS INLET	VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE MEASURED DIMENSIONLESS
1-2	6.40	12.3	335.7	368.9	315.3	1.19
1-4	6.40	12.3	335.7	368.9	315.3	1.46
1-5	6.40	12.3	335.7	368.9	315.3	1.94
1-6	6.40	12.3	335.7	368.9	315.3	2.35
1-7	6.40	12.3	335.7	368.9	315.3	2.70
1-8	6.40	12.3	335.7	368.9	315.3	2.97
1-9	6.40	12.3	335.7	368.9	315.3	3.14
1-10	6.40	12.3	335.7	368.9	315.3	3.29
1-11	6.40	12.3	335.7	368.9	315.3	3.44
1-12	6.40	12.3	335.7	368.9	315.3	3.59
1-13	6.40	12.3	335.7	368.9	315.3	3.74
1-14	6.40	12.3	335.7	368.9	315.3	3.89
1-15	6.40	12.3	335.7	368.9	315.3	4.04
1-16	6.40	12.3	335.7	368.9	315.3	4.19
1-17	6.40	12.3	335.7	368.9	315.3	4.34
1-18	6.40	12.3	335.7	368.9	315.3	4.49
1-19	6.40	12.3	335.7	368.9	315.3	4.64
1-20	6.40	12.3	335.7	368.9	315.3	4.79
1-21	6.40	12.3	335.7	368.9	315.3	4.94
1-22	6.40	12.3	335.7	368.9	315.3	5.09
1-23	6.40	12.3	335.7	368.9	315.3	5.24
1-24	6.40	12.3	335.7	368.9	315.3	5.39
1-25	6.40	12.3	335.7	368.9	315.3	5.54
1-26	6.40	12.3	335.7	368.9	315.3	5.69
1-27	6.40	12.3	335.7	368.9	315.3	5.84
1-28	6.40	12.3	335.7	368.9	315.3	5.99
1-29	6.40	12.3	335.7	368.9	315.3	6.14
1-30	6.40	12.3	335.7	368.9	315.3	6.29
1-31	6.40	12.3	335.7	368.9	315.3	6.44
1-32	6.40	12.3	335.7	368.9	315.3	6.59
1-33	6.40	12.3	335.7	368.9	315.3	6.74
1-34	6.40	12.3	335.7	368.9	315.3	6.89
1-35	6.40	12.3	335.7	368.9	315.3	7.04
1-36	6.40	12.3	335.7	368.9	315.3	7.19
1-37	6.40	12.3	335.7	368.9	315.3	7.34
1-38	6.40	12.3	335.7	368.9	315.3	7.49
1-39	6.40	12.3	335.7	368.9	315.3	7.64
1-40	6.40	12.3	335.7	368.9	315.3	7.79
1-41	6.40	12.3	335.7	368.9	315.3	7.94
1-42	6.40	12.3	335.7	368.9	315.3	8.09
1-43	6.40	12.3	335.7	368.9	315.3	8.24
1-44	6.40	12.3	335.7	368.9	315.3	8.39
1-45	6.40	12.3	335.7	368.9	315.3	8.54
1-46	6.40	12.3	335.7	368.9	315.3	8.69
1-47	6.40	12.3	335.7	368.9	315.3	8.84
1-48	6.40	12.3	335.7	368.9	315.3	8.99
1-49	6.40	12.3	335.7	368.9	315.3	9.14
50-1	6.40	12.3	335.7	368.9	315.3	9.29



575 139

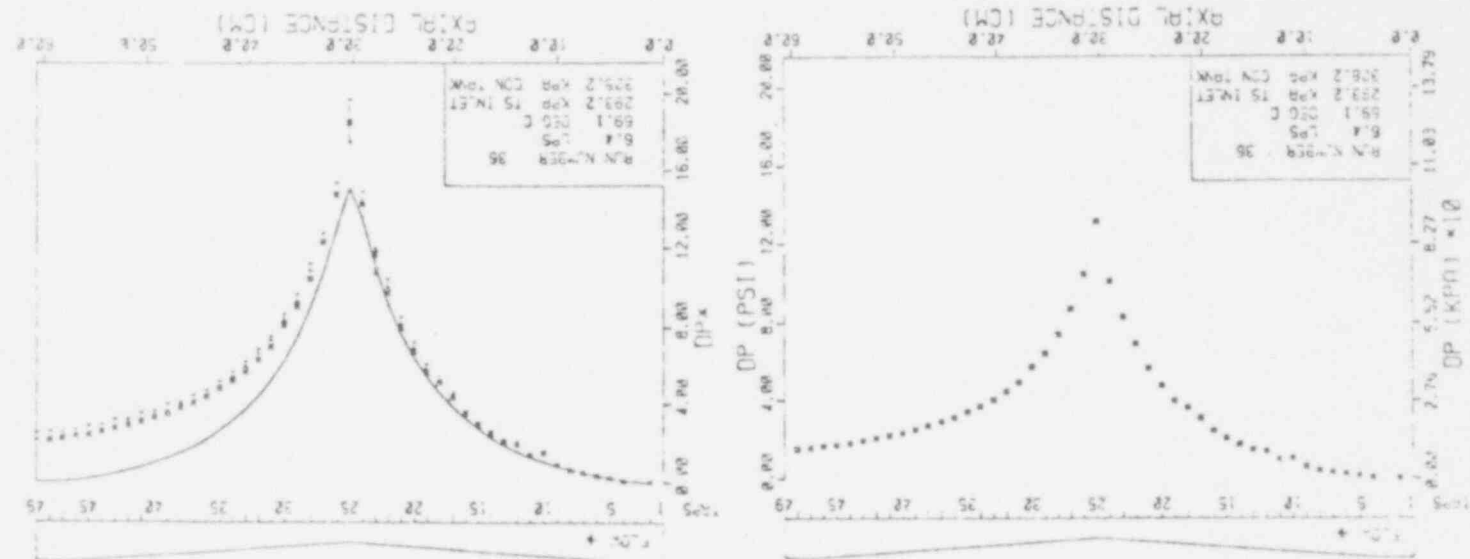
# POOR ORIGINAL

PL PRESSURE DATA FROM  
TEST SECTION # 2

RUN NUMBER 36

LOOP FLOW LTR/SEC TEMPERATURES (DBD C) PRESSURE (KPA) VELOCITY ROUNDS DIFFERENTIAL PRESSURE MEASUREMENT DIMENSIONS

50-1	6.38	66.1	308.2	314.4	.379E+06	1.9
1-69	6.38	66.1	293.2	314.4	.379E+06	1.9
1-48	6.38	66.1	293.2	314.4	.379E+06	1.9
1-47	6.38	66.1	293.2	314.4	.379E+06	1.9
1-45	6.38	66.1	293.2	314.4	.379E+06	1.9
1-44	6.38	66.1	293.2	314.4	.379E+06	1.9
1-43	6.38	66.1	293.2	314.4	.379E+06	1.9
1-42	6.38	66.1	293.2	314.4	.379E+06	1.9
1-41	6.38	66.1	293.2	314.4	.379E+06	1.9
1-40	6.38	66.1	293.2	314.4	.379E+06	1.9
1-39	6.38	66.1	293.2	314.4	.379E+06	1.9
1-38	6.38	66.1	293.2	314.4	.379E+06	1.9
1-37	6.38	66.1	293.2	314.4	.379E+06	1.9
1-36	6.38	66.1	293.2	314.4	.379E+06	1.9
1-35	6.38	66.1	293.2	314.4	.379E+06	1.9
1-34	6.38	66.1	293.2	314.4	.379E+06	1.9
1-33	6.38	66.1	293.2	314.4	.379E+06	1.9
1-32	6.38	66.1	293.2	314.4	.379E+06	1.9
1-31	6.38	66.1	293.2	314.4	.379E+06	1.9
1-30	6.38	66.1	293.2	314.4	.379E+06	1.9
1-29	6.38	66.1	293.2	314.4	.379E+06	1.9
1-28	6.38	66.1	293.2	314.4	.379E+06	1.9
1-27	6.38	66.1	293.2	314.4	.379E+06	1.9
1-26	6.38	66.1	293.2	314.4	.379E+06	1.9
1-25	6.38	66.1	293.2	314.4	.379E+06	1.9
1-24	6.38	66.1	293.2	314.4	.379E+06	1.9
1-23	6.38	66.1	293.2	314.4	.379E+06	1.9
1-22	6.38	66.1	293.2	314.4	.379E+06	1.9
1-21	6.38	66.1	293.2	314.4	.379E+06	1.9
1-20	6.38	66.1	293.2	314.4	.379E+06	1.9
1-19	6.38	66.1	293.2	314.4	.379E+06	1.9
1-18	6.38	66.1	293.2	314.4	.379E+06	1.9
1-17	6.38	66.1	293.2	314.4	.379E+06	1.9
1-16	6.38	66.1	293.2	314.4	.379E+06	1.9
1-15	6.38	66.1	293.2	314.4	.379E+06	1.9
1-14	6.38	66.1	293.2	314.4	.379E+06	1.9
1-13	6.38	66.1	293.2	314.4	.379E+06	1.9
1-12	6.38	66.1	293.2	314.4	.379E+06	1.9
1-11	6.38	66.1	293.2	314.4	.379E+06	1.9
1-10	6.38	66.1	293.2	314.4	.379E+06	1.9
1-9	6.38	66.1	293.2	314.4	.379E+06	1.9
1-8	6.38	66.1	293.2	314.4	.379E+06	1.9
1-7	6.38	66.1	293.2	314.4	.379E+06	1.9
1-6	6.38	66.1	293.2	314.4	.379E+06	1.9
1-5	6.38	66.1	293.2	314.4	.379E+06	1.9
1-4	6.38	66.1	293.2	314.4	.379E+06	1.9
1-3	6.38	66.1	293.2	314.4	.379E+06	1.9



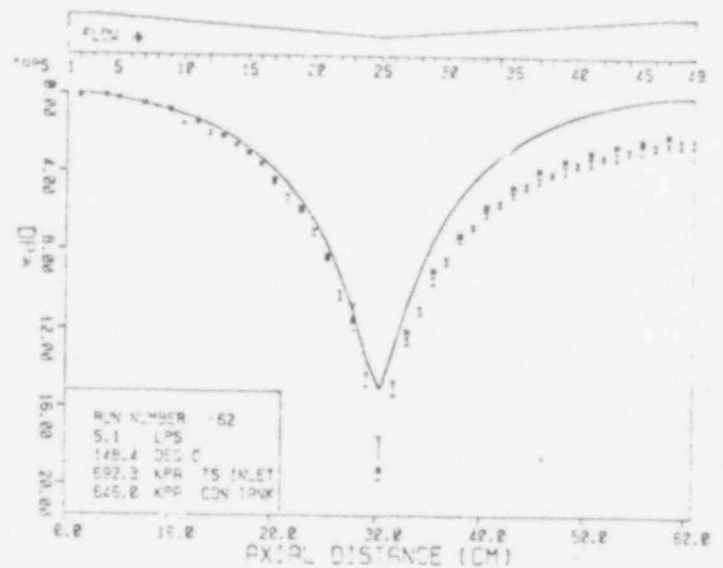
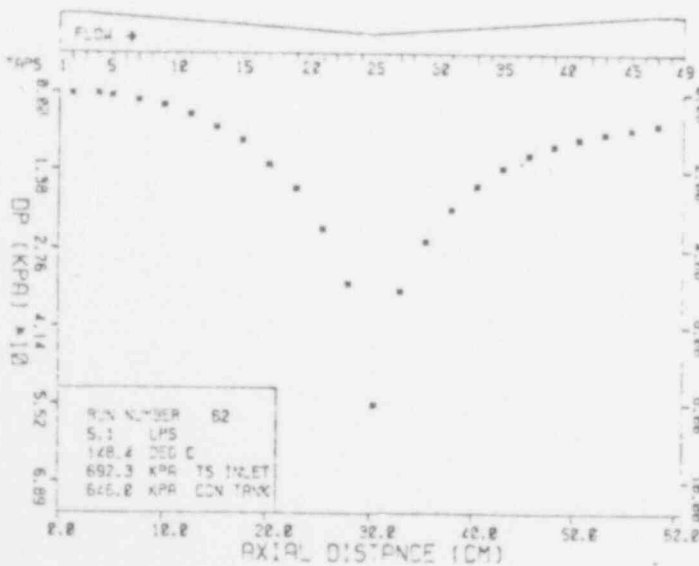
575 140

BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 62

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	5.06	131.6	148.5	148.5	692.3	646.0	249.0	616E+06	.33	.11
1-4	5.05	131.5	148.5	148.5	692.3	646.0	248.8	615E+06	.29	.10
1-5	5.06	131.5	148.5	148.4	692.3	646.0	249.2	616E+06	.63	.22
1-7	5.05	131.5	148.5	148.4	692.3	646.0	248.5	614E+06	1.35	.47
1-9	5.08	131.5	148.5	148.4	692.3	646.0	250.2	618E+06	2.27	.78
1-11	5.09	131.5	148.6	148.5	692.3	646.0	250.5	620E+06	4.01	1.38
1-13	5.08	131.5	148.5	148.5	692.3	646.0	250.3	619E+06	6.20	2.14
1-15	5.06	131.5	148.5	148.5	692.3	646.0	248.9	615E+06	8.56	2.94
1-17	5.09	131.5	148.6	148.5	692.3	646.0	250.7	620E+06	12.76	4.39
1-19	5.07	131.5	148.5	148.4	692.3	646.0	249.9	618E+06	16.88	5.84
1-21	5.08	131.5	148.5	148.4	692.3	646.0	250.1	618E+06	23.99	8.28
1-23	5.11	131.4	148.4	148.4	692.3	646.0	251.5	621E+06	33.62	11.48
1-25	5.07	131.4	148.5	148.4	692.3	646.0	249.6	617E+06	55.39	19.20
1-27	5.08	131.4	148.4	148.4	692.3	646.0	250.1	618E+06	35.01	12.09
1-29	5.09	131.4	148.6	148.4	692.3	646.0	250.8	620E+06	26.19	9.08
1-31	5.04	131.4	148.4	148.4	692.3	646.0	248.3	613E+06	21.58	7.21
1-33	5.08	131.4	148.4	148.4	692.3	646.0	249.9	618E+06	16.51	5.71
1-35	5.06	131.4	148.5	148.4	692.3	646.0	249.0	615E+06	13.37	4.66
1-37	5.09	131.3	148.5	148.4	692.3	646.0	250.5	619E+06	11.10	3.92
1-39	5.08	131.4	148.4	148.4	692.3	646.0	250.2	618E+06	9.54	3.29
1-41	5.08	131.3	148.4	148.4	692.3	646.0	249.9	617E+06	8.19	2.83
1-43	5.09	131.3	148.6	148.4	692.3	646.0	250.7	620E+06	7.25	2.49
1-45	5.05	131.3	148.5	148.4	692.3	646.0	248.7	615E+06	6.41	2.24
1-47	5.06	131.3	148.5	148.4	692.3	646.0	249.0	616E+06	5.66	1.97
1-49	5.08	131.3	148.4	148.4	692.3	646.0	250.0	618E+06	5.35	1.85
50"	5.06	131.3	148.4	148.4	692.3	646.0	249.4	616E+06	2.71	.94

POOR ORIGINAL







APPENDIX B

PRESSURE DISTRIBUTION DATA UNDER FLASHING CONDITIONS

SOME PHOTOGRAPHIC OBSERVATIONS

B. FLASHING EXPERIMENTS

RUN	$P_{in}$ (kPa)	$T_{in}$ ( $^{\circ}$ C)	$G$ (Mg/m <sup>2</sup> s)	$P_{ct}$ (kPa)	$T_{ct}$ ( $^{\circ}$ C)
20	281.	98.3	4.90	245.	98.2
21	393.	100.6	6.01	136.	100.4
22	170.	100.2	3.04	125.	100.1
23	130.	99.4	1.81	121.	99.3
24	160.	98.0	3.05	122.	97.8
25	247.	97.4	4.52	125.	97.3
26	386.	97.8	6.02	132.	97.7
27	326.	130.0	2.95	299.	129.6
28	566.	131.7	5.90	316.	131.4
29	488.	123.5	5.77	210.	115.4
30	375.	125.1	4.50	206.	114.7
31	----	-----	----	----	-----
35	287.	99.4	4.96	250.	99.2
37	296.	100.3	4.94	170.	100.0
38	117.	100.3	2.05	112.	99.8
39	136.	100.5	2.25	112.	100.1
40	168.	100.3	3.02	112.	100.0
41	250.	100.2	4.54	115.	99.8
42	194.	99.6	3.79	114.	99.4
43	287.	100.2	4.97	121.	99.9
44	271.	99.9	4.50	101.	99.9
45	308.	99.8	4.97	99.	100.0
46	223.	99.9	3.79	99.	99.9
47	----	-----	----	----	-----

B. FLASHING EXPERIMENTS

(Cont'd)

RUN	$P_{in}$ (kPa)	$T_{in}$ ( $^{\circ}$ C)	$G$ (Mg/m <sup>2</sup> s)	$P_{ct}$ (kPa)	$T_{ct}$ ( $^{\circ}$ C)
48	183.	99.9	3.04	100	99.9
49	146.	99.9	2.27	99	99.7
50	142.	99.8	2.04	101	99.9
51	----	-----	----	---	-----
52	381.	123.5	4.48	254	123.5
53	395.	123.6	4.45	249	123.6
54	525.	123.6	5.96	252	123.7
55	293.	123.6	2.99	251	123.6
56	261.	123.2	2.20	252	123.6
57	263.	124.7	2.04	256	123.9
58	254.	123.3	2.98	174	110.2
59	254.	123.1	2.98	174	110.2
60	264.	125.8	2.93	186	112.5
61	259.	123.8	2.98	162	108.8
63	739.	148.7	5.85	464	148.7
64	609.	148.8	4.40	463	148.8
65	----	-----	----	---	-----
66	521.	148.8	2.94	463	148.8
67	502.	148.6	2.22	463	148.7
68	395.	143.5	1.24	185	118.0
69	399.	144.3	1.23	188	118.5

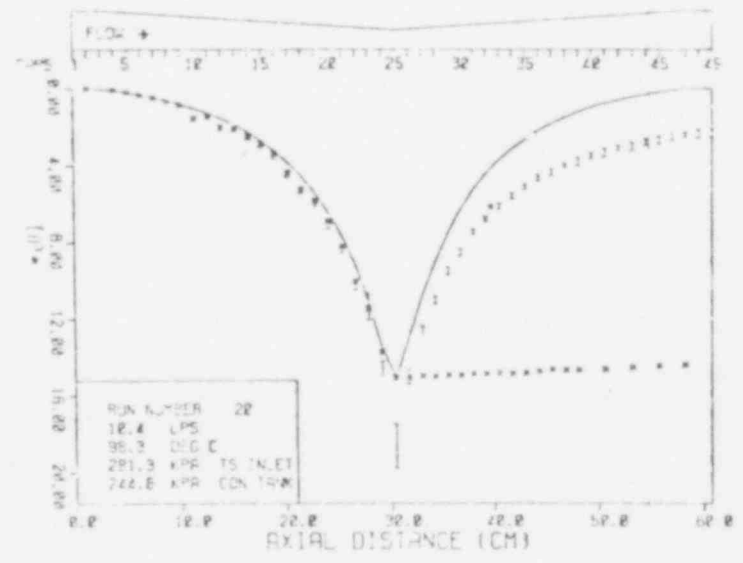
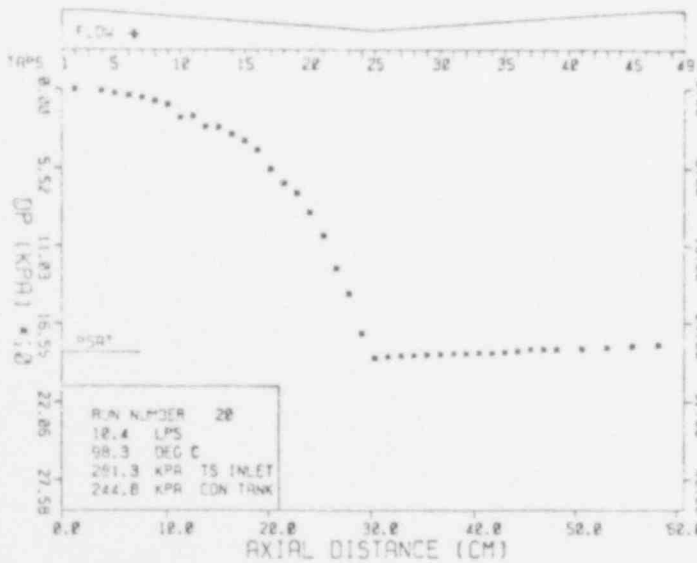


BNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER 20

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	.18	.01
1-4	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	1.18	.09
1-5	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	2.68	.21
1-6	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	4.48	.36
1-7	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	6.16	.49
1-8	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	8.20	.65
1-9	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	10.67	.85
1-10	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	19.53	1.55
1-11	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	18.48	1.47
1-12	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	25.84	2.05
1-13	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	26.56	2.11
1-14	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	31.27	2.49
1-15	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	35.95	2.86
1-16	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	42.21	3.35
1-17	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	55.72	4.43
1-18	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	65.63	5.22
1-19	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	72.65	5.77
1-20	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	86.34	6.86
1-21	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	102.88	8.18
1-22	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	126.31	10.04
1-23	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	144.23	11.46
1-24	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	172.69	13.72
1-25	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	189.80	15.08
1-26	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	188.92	15.01
1-27	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	188.31	14.96
1-28	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	188.49	14.98
1-29	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	187.86	14.93
1-30	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	187.43	14.89
1-31	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	186.72	14.84
1-32	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	186.74	14.84
1-33	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	186.26	14.80
1-34	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	186.38	14.81
1-35	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	185.88	14.77
1-36	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	184.96	14.70
1-37	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	183.85	14.61
1-38	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	183.97	14.62
1-39	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	183.95	14.62
1-41	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	183.66	14.59
1-43	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	182.52	14.50
1-45	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	181.48	14.42
1-47	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	180.60	14.35
1-49	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	179.89	14.29
50-1	10.36	99.4	98.3	98.2	281.3	244.8	510.1	.856E+06	17.24	1.37

POOR ORIGINAL



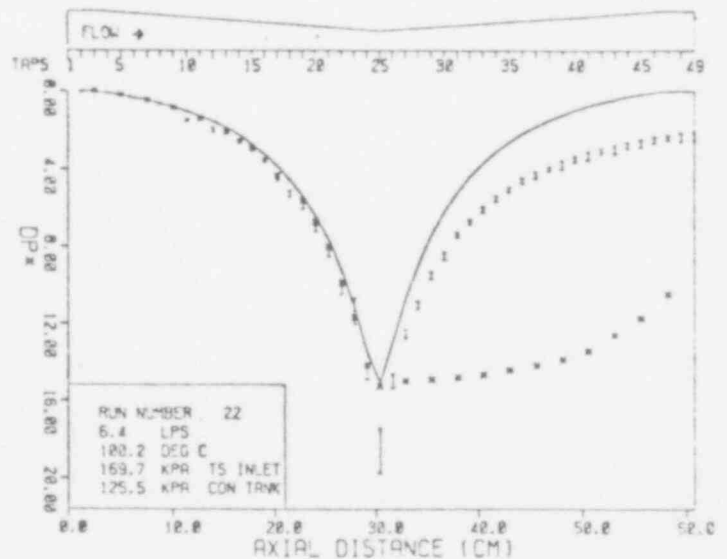
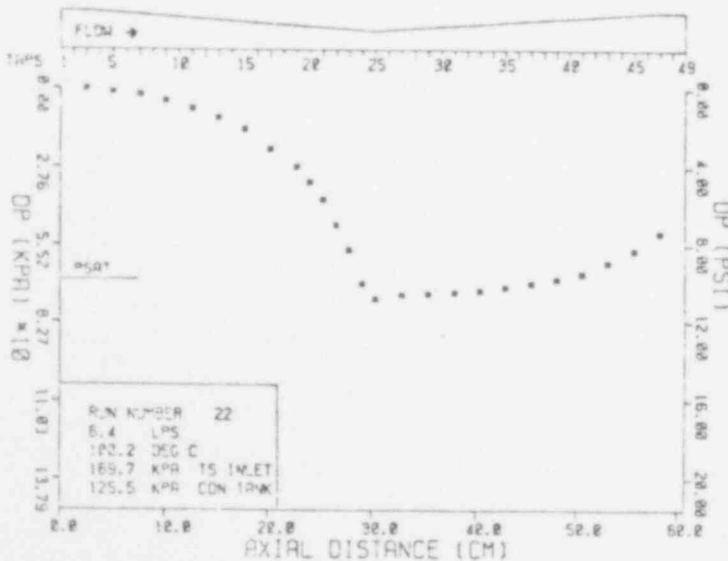


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 22

TAPS	LOOP FLOW LTR/SUC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM/SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-3	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	.03	.01
1-5	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	1.08	.22
1-7	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	2.26	.47
1-9	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	4.10	.84
1-11	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	6.85	1.41
1-13	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	10.21	2.10
1-15	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	14.13	2.91
1-17	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	21.10	4.34
1-19	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	27.37	5.62
1-20	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	32.68	6.73
1-21	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	38.82	7.99
1-22	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	47.79	9.84
1-23	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	56.71	11.67
1-24	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	68.78	14.16
1-25	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	74.13	15.26
1-27	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	72.84	14.99
1-29	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	72.52	14.93
1-29	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	72.03	14.83
1-31	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	71.36	14.69
1-33	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	70.19	14.45
1-35	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	68.95	14.19
1-37	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	67.46	13.89
1-39	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	65.27	13.43
1-41	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	61.18	12.59
1-43	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	56.98	11.73
1-45	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	50.78	10.45
1-47	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	45.86	9.44
1-49	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06	6.09	1.25
50-1	6.44	100.0	100.2	100.1	169.7	125.5	317.2	.542E+06		

POOR ORIGINAL

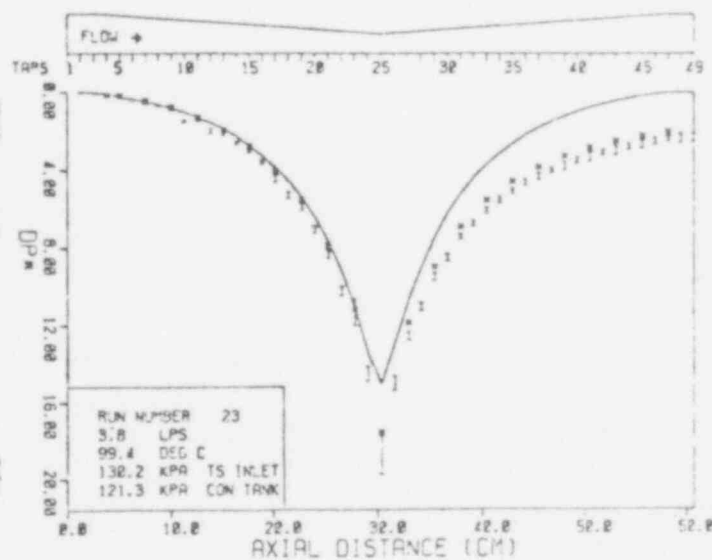
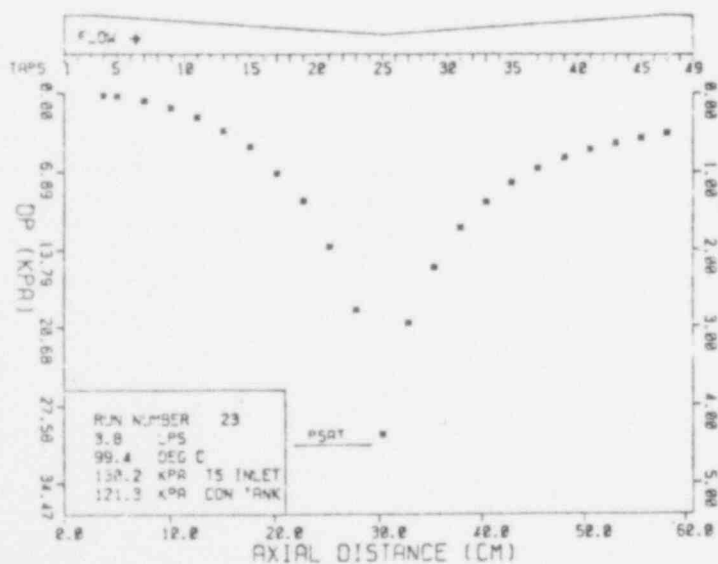


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 23

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-4	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	.25	.14
1-5	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	.31	.18
1-7	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	.71	.41
1-9	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	1.38	.76
1-11	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	2.14	1.25
1-13	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	3.26	1.90
1-15	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	4.65	2.72
1-17	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	6.99	4.08
1-19	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	9.41	5.50
1-21	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	13.48	7.87
1-23	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	19.14	11.18
1-25	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	30.14	17.60
1-27	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	20.03	11.87
1-29	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	15.39	8.99
1-31	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	11.84	6.91
1-33	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	9.56	5.58
1-35	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	7.81	4.56
1-37	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	6.57	3.84
1-39	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	5.61	3.28
1-41	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	4.88	2.85
1-43	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	4.33	2.53
1-45	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	3.88	2.27
1-47	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	3.48	2.03
1-49	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	3.33	1.94
50-1	3.82	100.3	99.4	99.3	130.2	121.3	188.3	.319E+06	1.47	.86

POOR ORIGINAL

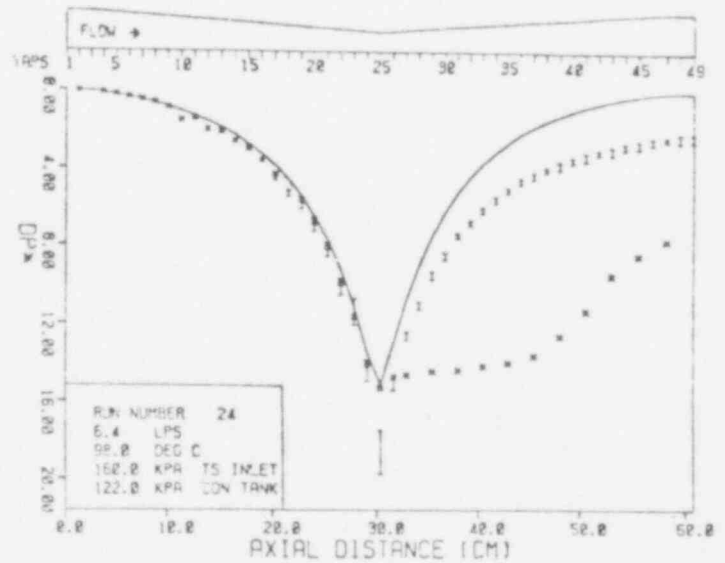
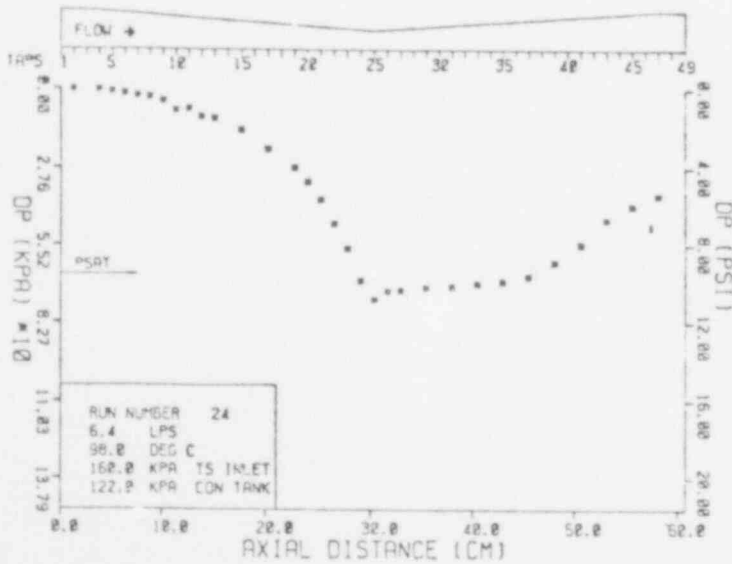


BNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER 24

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	.10	.02
1-4	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	.45	.09
1-5	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	.94	.19
1-6	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	1.65	.34
1-7	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	2.28	.47
1-8	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	2.86	.59
1-9	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	4.07	.84
1-10	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	7.25	1.49
1-11	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	6.77	1.39
1-12	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	9.54	1.96
1-13	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	10.07	2.07
1-15	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	14.13	2.90
1-17	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	20.84	4.28
1-19	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	27.25	5.60
1-20	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	32.34	6.65
1-21	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	38.67	7.95
1-22	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	47.42	9.74
1-23	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	56.43	11.59
1-24	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	67.86	13.94
1-25	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	74.27	15.26
1-26	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	71.37	14.67
1-27	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	71.05	14.60
1-29	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	70.13	14.41
1-31	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	69.78	14.34
1-33	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	68.73	14.12
1-35	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	67.80	13.93
1-37	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	66.18	13.60
1-39	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	61.16	12.57
1-41	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	54.84	11.27
1-43	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	45.93	9.44
1-45	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	41.00	8.42
1-47	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	37.29	7.66
1-49	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	35.89	7.37
50-1	6.44	98.7	98.0	97.8	160.0	122.0	317.2	.531E+06	5.91	1.21

POOR ORIGINAL



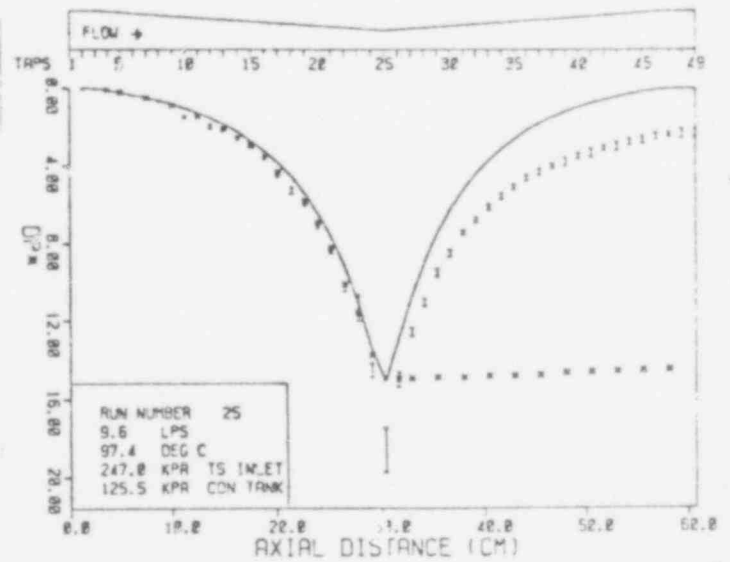
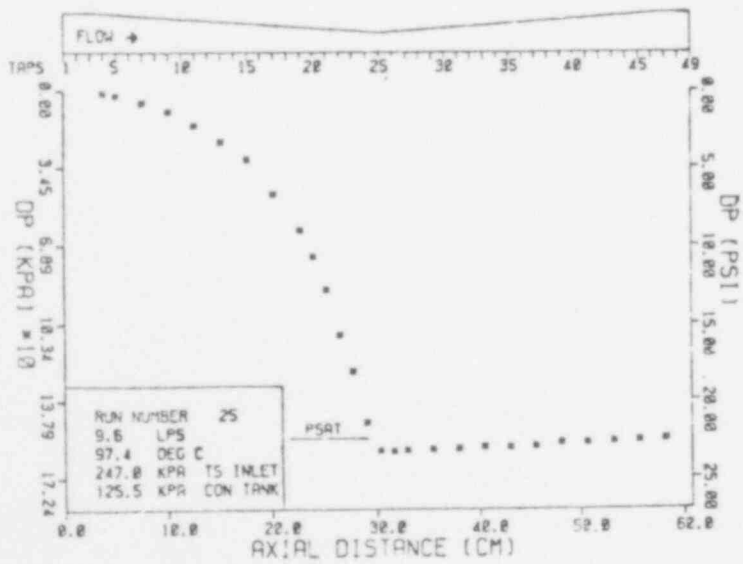
575 151

BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 25

TAPS	LOOP FLOW LTR/SHR	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-4	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	1.14	.11
1-5	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	2.25	.21
1-7	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	5.34	.50
1-9	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	9.31	.87
1-11	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	15.59	1.46
1-13	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	22.90	2.14
1-15	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	30.85	2.88
1-17	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	46.15	4.31
1-19	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	62.68	5.80
1-20	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	73.82	6.89
1-21	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	88.02	8.22
1-22	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	108.09	10.10
1-23	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	124.44	11.62
1-24	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	147.60	13.79
1-25	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	160.01	14.95
1-26	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	160.29	14.97
1-27	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	159.81	14.93
1-29	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	159.39	14.89
1-31	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	159.20	14.87
1-33	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	158.48	14.80
1-35	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	158.43	14.80
1-37	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	157.99	14.76
1-39	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	156.75	14.64
1-41	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	156.48	14.62
1-43	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	156.08	14.58
1-45	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	155.71	14.54
1-47	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	154.28	14.49
1-49	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	154.28	14.41
50-1	9.55	98.2	97.4	97.3	247.0	125.5	470.3	.783E+06	14.99	1.40

POOR ORIGINAL

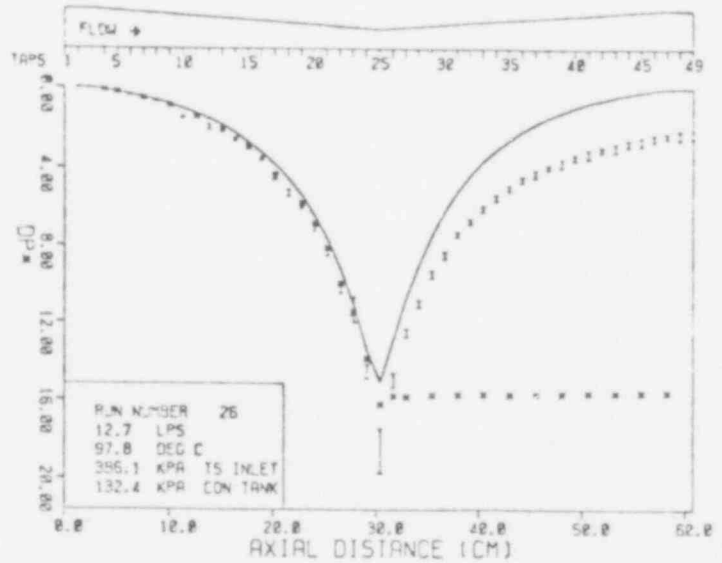
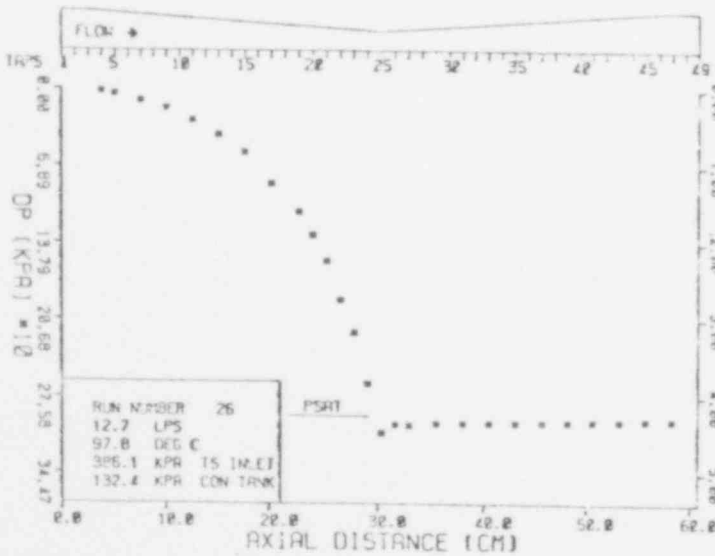


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 26

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM/SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-4	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	2.10	.11
1-5	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	4.08	.22
1-7	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	9.97	.53
1-9	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	16.38	.86
1-11	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	27.41	1.45
1-13	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	40.23	2.12
1-15	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	56.24	2.97
1-17	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	84.25	4.44
1-19	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	109.41	5.77
1-20	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	130.22	6.67
1-21	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	153.77	8.11
1-23	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	189.02	9.97
1-24	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	218.18	11.51
1-25	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	263.39	13.89
1-26	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	307.60	16.32
1-27	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	349.96	18.82
1-28	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	390.60	21.35
1-29	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	428.98	23.77
1-31	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	464.94	25.77
1-33	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	498.59	27.35
1-35	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	529.88	28.55
1-37	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	558.30	29.73
1-39	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	584.75	30.70
1-41	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	609.36	31.68
1-43	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	632.4	32.49
1-45	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	654.36	33.13
1-47	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	674.48	33.64
1-49	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	694.85	34.05
50-1	12.71	98.6	97.8	97.7	386.1	132.4	626.0	.105E+07	26.86	1.42

POOR ORIGINAL



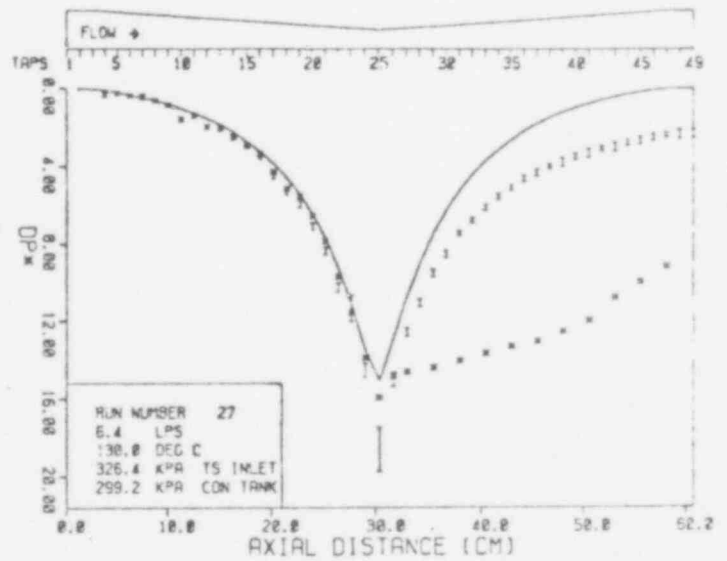
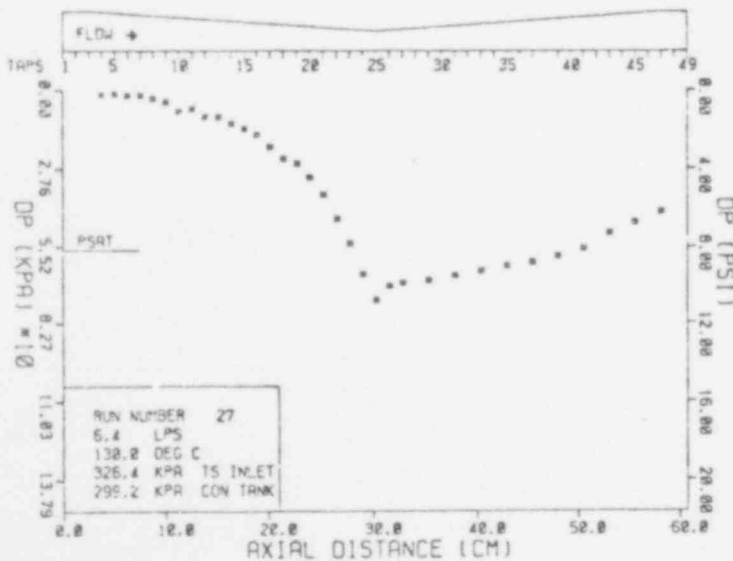
575 153

BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 27

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE MEASURED DIMENSIONLESS	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK				
1-4	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	1.59	.34
1-5	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	1.29	.28
1-6	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	1.77	.38
1-7	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	1.84	.39
1-8	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	2.90	.62
1-9	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	4.01	.86
1-10	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	7.45	1.59
1-11	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	6.50	1.29
1-12	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	9.17	1.96
1-13	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	9.34	2.00
1-14	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	11.76	2.52
1-15	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	13.55	2.90
1-16	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	15.63	3.34
1-17	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	19.88	4.25
1-18	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	23.97	5.13
1-19	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	25.69	5.50
1-20	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	30.53	6.53
1-21	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	36.63	7.84
1-22	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	45.26	9.68
1-23	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	53.92	11.54
1-24	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	64.96	13.90
1-25	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	74.52	15.94
1-26	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	69.31	14.83
1-27	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	68.23	14.60
1-29	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	67.18	14.37
1-31	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	65.55	14.02
1-33	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	63.78	13.64
1-35	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	62.09	13.28
1-37	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	60.84	13.02
1-39	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	58.56	12.53
1-41	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	55.86	11.95
1-43	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	50.35	10.77
1-45	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	46.43	9.93
1-47	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	42.77	9.15
1-49	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	39.16	8.38
50-1	6.40	130.9	130.0	129.6	326.4	299.2	315.0	.687E+06	5.19	1.11

POOR ORIGINAL



575  
959

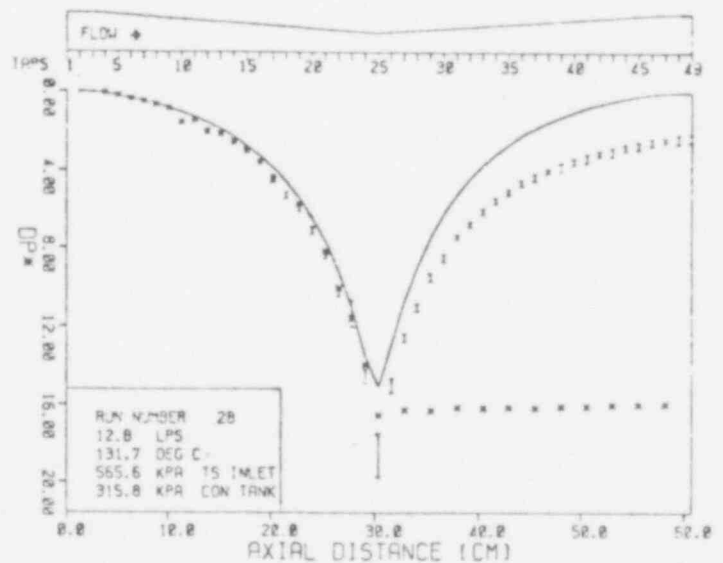
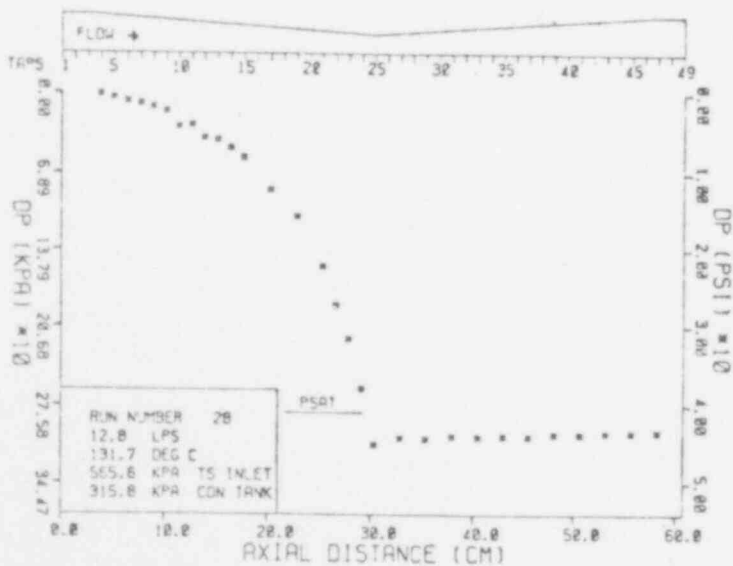


BML FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 28

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-4	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	1.33	.07
1-5	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	3.63	.19
1-6	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	6.73	.36
1-7	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	9.01	.48
1-8	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	11.79	.63
1-9	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	15.47	.83
1-10	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	28.65	1.53
1-11	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	27.08	1.45
1-12	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	38.12	2.04
1-13	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	40.03	2.14
1-14	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	46.84	2.50
1-15	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	55.23	2.95
1-17	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	83.32	4.45
1-21	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	107.42	5.74
1-22	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	152.63	8.16
1-23	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	187.88	10.04
1-24	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	217.10	11.61
1-25	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	267.64	13.93
1-27	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	309.54	16.55
1-29	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	304.19	16.26
1-31	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	304.79	16.29
1-33	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	302.19	16.15
1-35	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	302.74	16.18
1-37	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	302.03	16.15
1-39	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	302.21	16.16
1-41	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	300.67	16.07
1-43	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	300.72	16.09
1-45	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	299.76	16.02
1-47	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	299.40	16.01
1-49	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	298.92	15.98
50-1	12.81	132.6	131.7	131.4	565.6	315.8	630.7	.139E+07	300.03	16.04
									27.33	1.46

POOR ORIGINAL

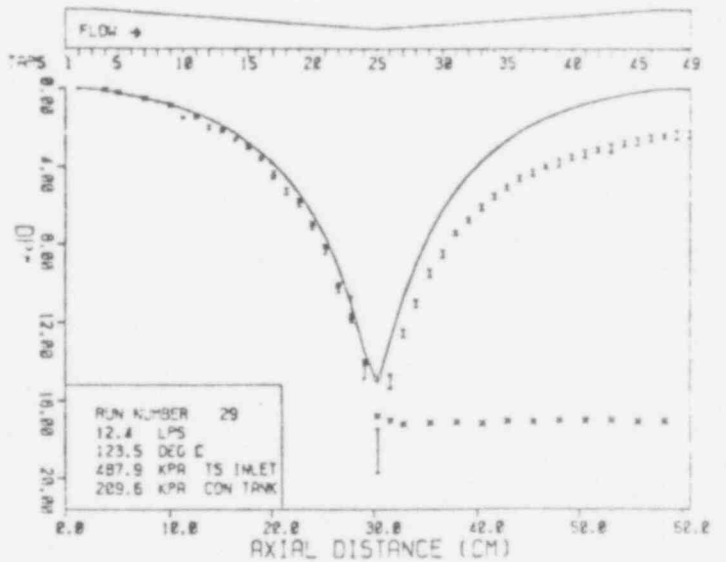
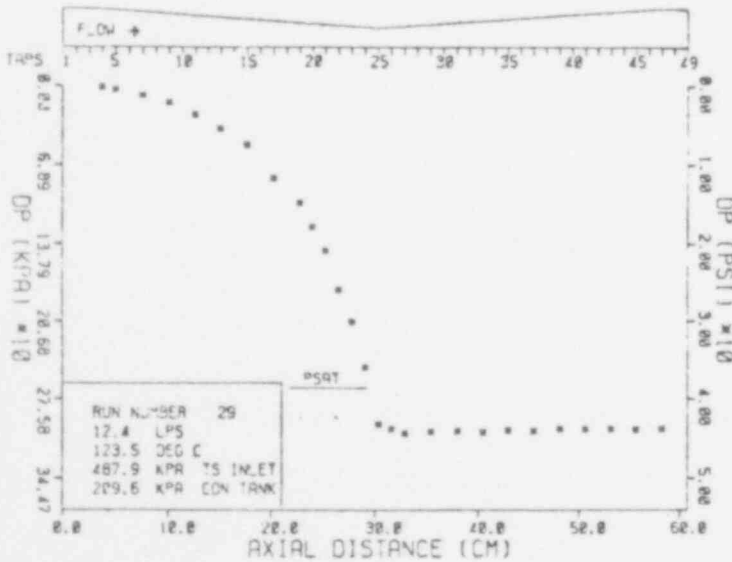


BML FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 29

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-4	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	1.34	.08
1-5	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	3.53	.20
1-7	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	8.72	.43
1-9	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	14.72	.60
1-11	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	25.46	1.44
1-13	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	37.96	2.14
1-15	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	51.39	2.90
1-17	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	60.42	4.53
1-19	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	101.99	5.75
1-20	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	122.94	6.93
1-21	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	143.86	8.11
1-22	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	179.00	10.09
1-23	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	207.35	11.69
1-24	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	247.89	13.58
1-25	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	297.85	16.79
1-26	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	302.14	17.04
1-27	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	305.46	17.22
1-29	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	303.91	17.14
1-31	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	303.61	17.12
1-33	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	304.79	17.19
1-35	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	302.93	17.08
1-37	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	303.39	17.11
1-39	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	301.79	17.02
1-41	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	302.05	17.03
1-43	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	301.53	17.00
1-45	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	302.46	17.05
1-47	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	302.12	17.04
1-49	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	302.01	17.03
50-1	12.42	116.6	123.5	115.4	487.9	209.6	611.7	.127E+07	26.47	1.09

POOR ORIGINAL

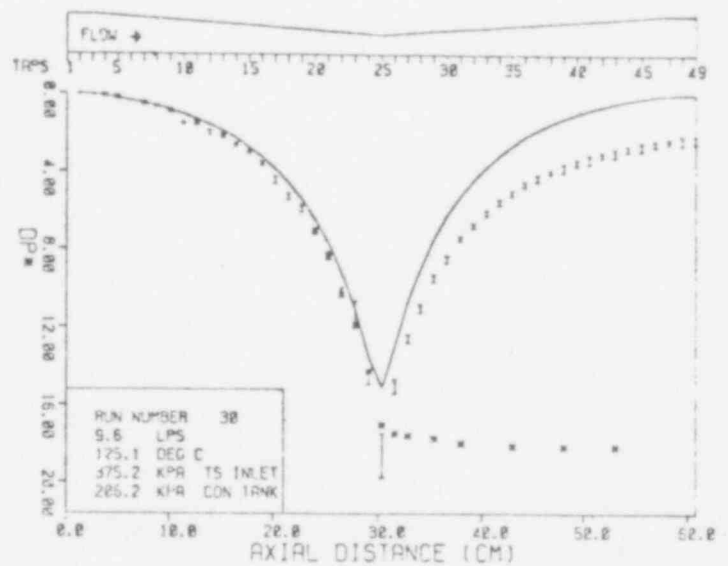
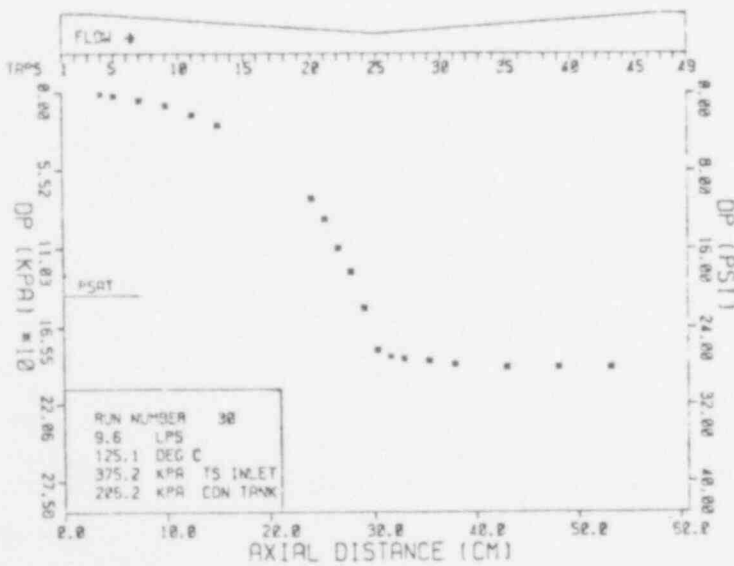


BNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER 30

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-4	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	1.00	.10
1-5	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	2.17	.20
1-7	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	5.25	.49
1-9	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	9.22	.86
1-11	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	15.79	1.46
1-13	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	23.15	2.17
1-20	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	75.00	7.03
1-21	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	89.44	8.39
1-22	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	110.14	10.33
1-23	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	126.62	11.87
1-24	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	151.55	14.21
1-25	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	181.46	17.02
1-26	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	186.22	17.46
1-27	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	187.46	17.59
1-29	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	188.98	17.72
1-31	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	191.73	17.98
1-35	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	193.50	18.15
1-39	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	193.75	18.17
1-43	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	193.84	18.18
1-49	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	193.72	18.17
50-1	9.64	115.9	125.1	114.7	375.2	206.2	474.7	.999E+06	15.07	1.41

**POOR ORIGINAL**

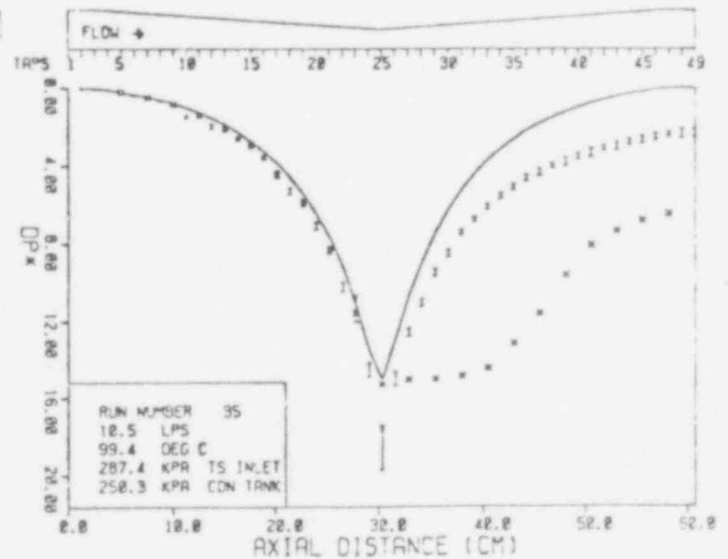
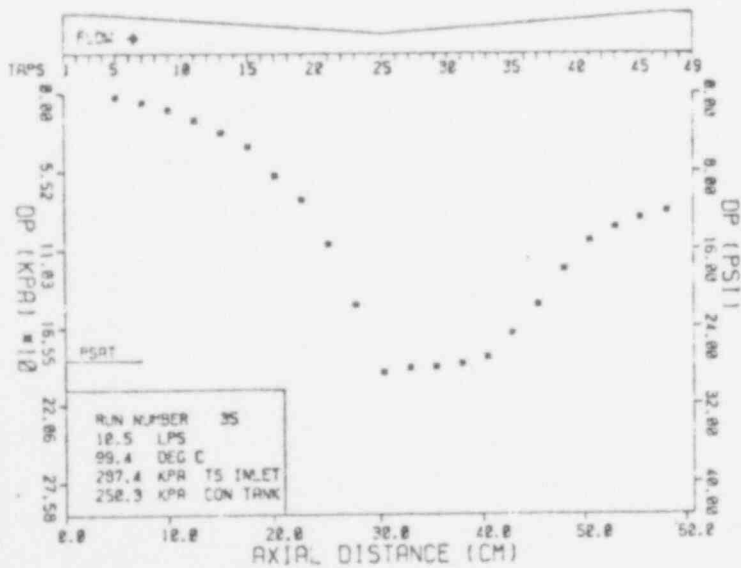


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 35

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-5	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	2.60	.20
1-7	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	6.32	.49
1-9	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	11.17	.87
1-11	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	18.41	1.43
1-13	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	27.23	2.11
1-15	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	37.09	2.88
1-17	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	57.50	4.46
1-19	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	74.81	5.81
1-21	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	106.25	8.25
1-23	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	148.86	11.56
1-25	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	197.05	15.30
1-27	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	194.09	15.07
1-29	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	193.61	15.03
1-31	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	191.61	14.87
1-33	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	186.57	14.48
1-35	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	169.89	13.19
1-37	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	149.13	11.58
1-39	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	124.04	9.67
1-41	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	104.18	8.09
1-43	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	94.80	7.36
1-45	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	87.98	6.83
1-47	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	83.36	6.47
1-49	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	82.60	6.41
50-1	10.49	96.6	99.4	99.2	287.4	250.3	516.3	.876E+06	18.06	1.40

POOR ORIGINAL

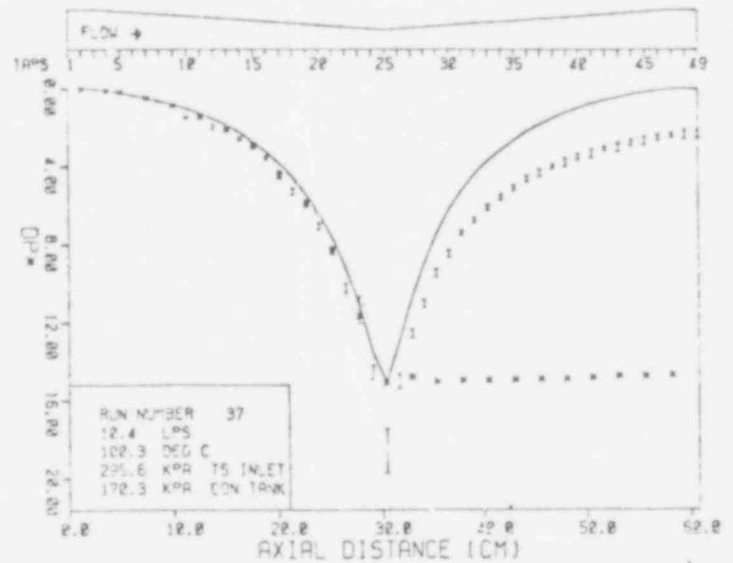
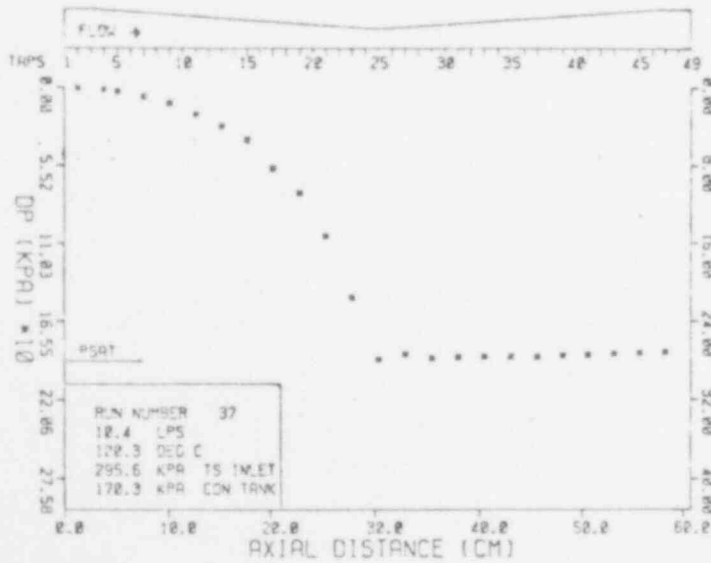


BNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER 37

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM/SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	.55	.04
1-4	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	1.43	.11
1-5	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	2.68	.21
1-7	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	6.36	.50
1-9	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	11.03	.86
1-11	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	18.75	1.47
1-13	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	26.96	2.11
1-15	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	36.75	2.88
1-17	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	57.09	4.47
1-19	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	74.46	5.83
1-21	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	105.08	8.23
1-23	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	148.72	11.65
1-25	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	192.64	15.09
1-27	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	238.92	18.80
1-29	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	291.68	23.02
1-31	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	349.19	27.58
1-33	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	410.64	32.34
1-35	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	476.37	37.31
1-37	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	546.30	42.51
1-39	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	620.81	48.07
1-41	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	699.26	53.93
1-43	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	781.23	60.17
1-45	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	867.95	66.75
1-47	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	959.40	73.68
1-49	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	1055.95	80.97
50-1	10.44	97.4	100.3	100.0	295.6	170.3	514.2	.879E+06	18.06	1.42

POOR ORIGINAL

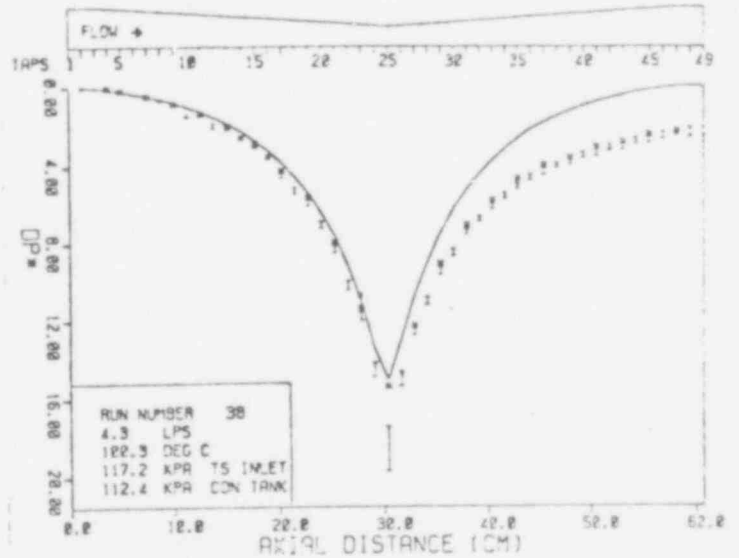
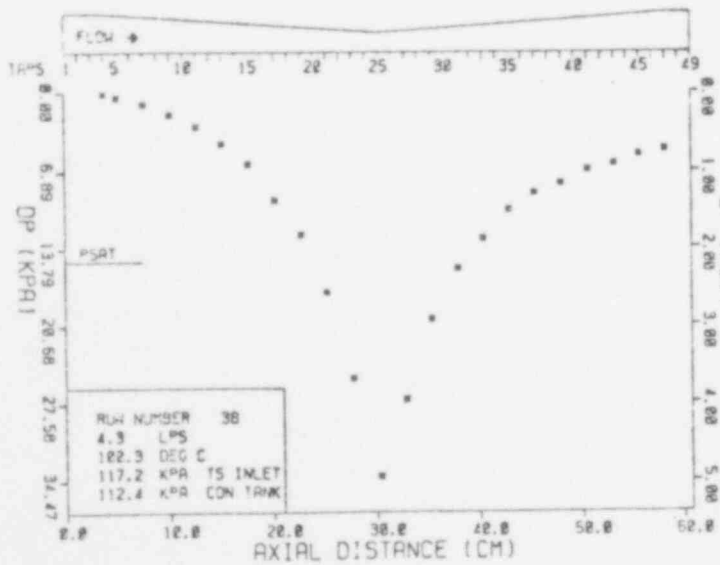


BML PLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 38

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW WATER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-4	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	.14	.06
1-5	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	.46	.21
1-7	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	1.04	.47
1-9	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	1.90	.86
1-11	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	2.98	1.35
1-13	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	4.48	2.03
1-15	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	6.25	2.82
1-17	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	9.38	4.24
1-19	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	12.48	5.64
1-21	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	17.63	7.98
1-23	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	25.37	11.47
1-25	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	34.06	15.40
1-25	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	27.23	12.31
1-27	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	20.13	9.10
1-29	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	15.65	7.08
1-31	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	12.89	5.83
1-33	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	10.34	4.68
1-35	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	8.83	3.99
1-37	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	8.00	3.62
1-39	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	6.83	3.09
1-41	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	6.27	2.84
1-43	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	5.45	2.46
1-45	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	5.03	2.28
1-47	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	5.10	2.31
1-49	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06	2.76	1.25
50-1	4.35	93.3	100.3	99.8	117.2	112.4	214.0	.366E+06		

POOR ORIGINAL

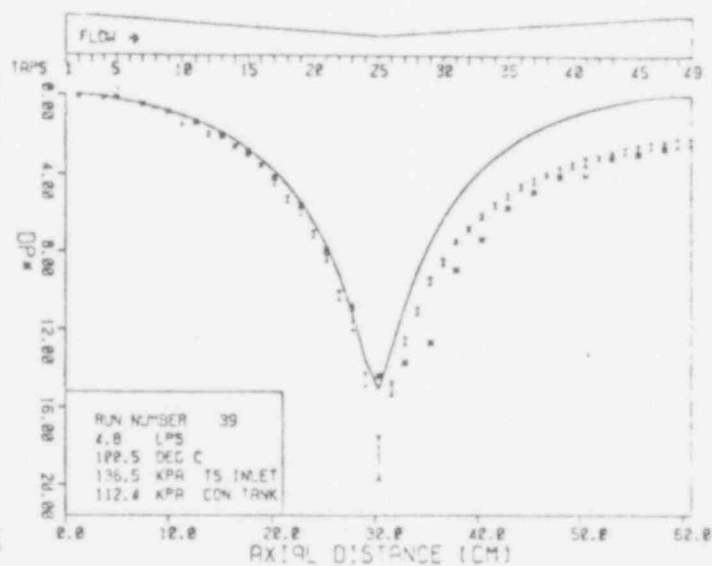
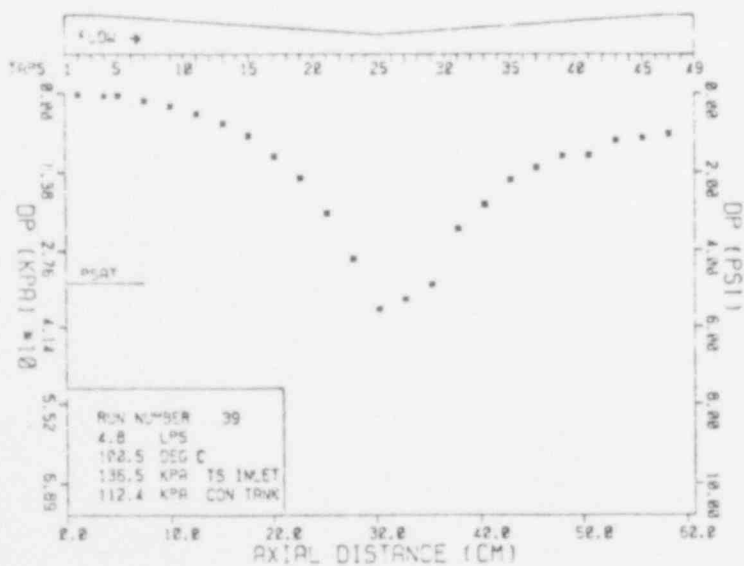


BNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER 39

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM/SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	.21	.08
1-4	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	.41	.16
1-5	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	.43	.16
1-7	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	1.29	.49
1-9	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	2.25	.85
1-11	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	3.58	1.35
1-13	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	5.39	2.03
1-15	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	7.45	2.80
1-17	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	11.03	4.15
1-19	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	14.75	5.56
1-21	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	20.96	7.89
1-23	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	28.96	10.90
1-25	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	38.13	14.36
1-27	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	36.34	13.68
1-29	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	33.65	12.67
1-31	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	23.72	8.93
1-33	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	19.44	7.32
1-35	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	15.10	5.69
1-37	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	12.96	4.89
1-39	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	10.89	4.10
1-41	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	10.82	4.08
1-43	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	8.70	3.19
1-45	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	7.79	2.93
1-47	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	7.10	2.67
1-49	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	6.89	2.60
50-1	4.76	93.6	100.5	100.1	136.5	112.4	234.6	.402E+06	3.10	1.17

POOR ORIGINAL

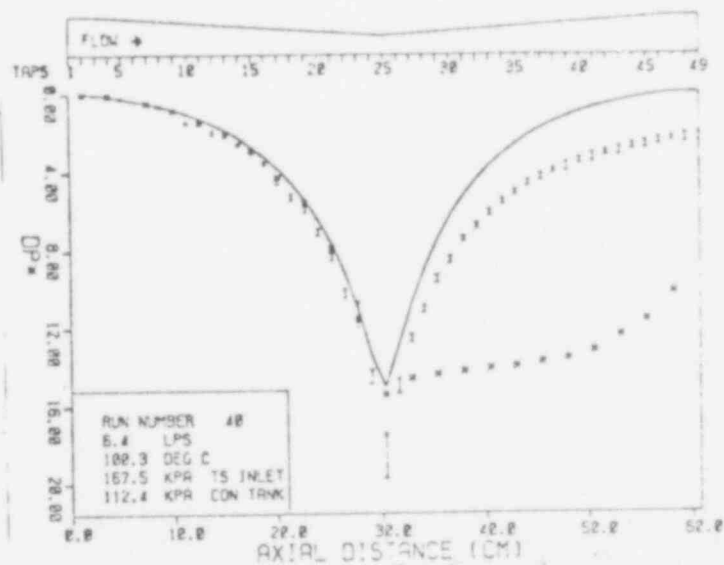
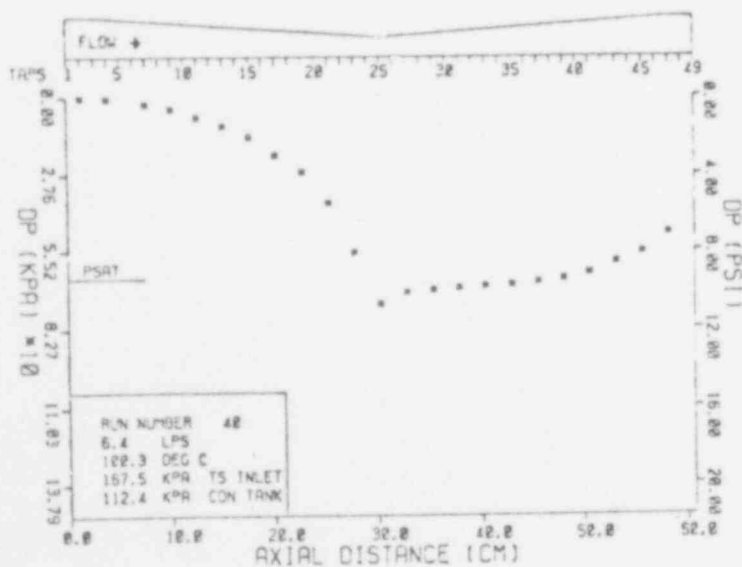


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 40

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	.18	.04
1-4	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	.42	.09
1-7	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	2.32	.48
1-9	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	4.10	.86
1-11	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	7.03	1.47
1-13	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	9.93	2.08
1-15	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	13.79	2.88
1-17	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	20.48	4.28
1-19	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	26.48	5.54
1-21	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	37.78	7.90
1-23	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	55.50	11.61
1-25	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	73.84	15.44
1-27	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	69.91	14.62
1-29	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	63.02	14.43
1-31	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	68.26	14.27
1-33	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	67.64	14.15
1-35	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	67.16	14.04
1-37	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	66.12	13.93
1-39	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	65.22	13.84
1-41	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	63.29	13.74
1-43	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	59.43	12.43
1-45	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	55.71	11.85
1-47	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	48.75	10.19
1-49	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	44.40	9.29
50-1	6.39	95.6	100.3	100.0	167.5	112.4	314.7	.539E+06	5.52	1.15

POOR ORIGINAL



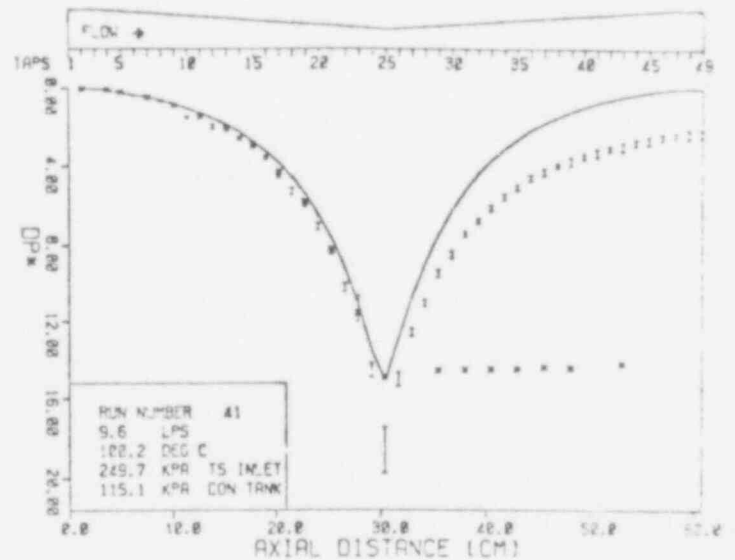
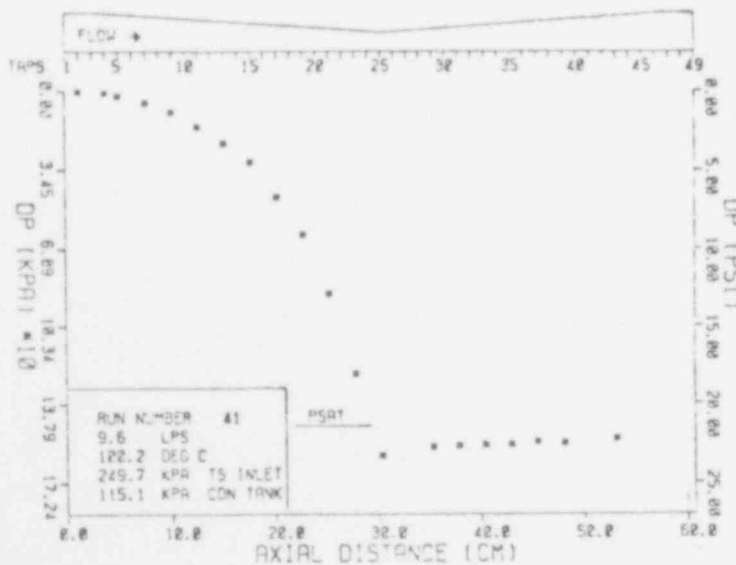


BMI FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 41

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)		PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE		
		FLOW METER	TS INLET	COND TANK	TS INLET			COND TANK	MEASURED	DIMENSIONLESS
1-2	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	.36	.03
1-4	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	.97	.09
1-5	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	2.16	.20
1-7	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	5.25	.49
1-9	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	9.39	.87
1-11	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	15.65	1.45
1-13	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	22.96	2.13
1-15	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	30.90	2.87
1-17	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	40.26	3.79
1-19	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	52.60	5.81
1-21	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	69.01	8.26
1-23	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	94.83	11.58
1-25	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	124.83	14.90
1-27	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	160.65	18.56
1-29	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	196.99	22.52
1-31	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	246.58	28.47
1-33	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	301.03	34.48
1-35	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	362.72	41.35
1-37	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	428.04	48.41
1-39	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	500.41	56.23
1-43	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	628.06	68.20
1-49	9.60	96.9	100.2	99.8	249.7	115.1	472.5	.808E+06	815.10	89.00
50-1	9.60	96.9	100.2	99.8	249.7	115.1	172.5	.808E+06		

POOR ORIGINAL

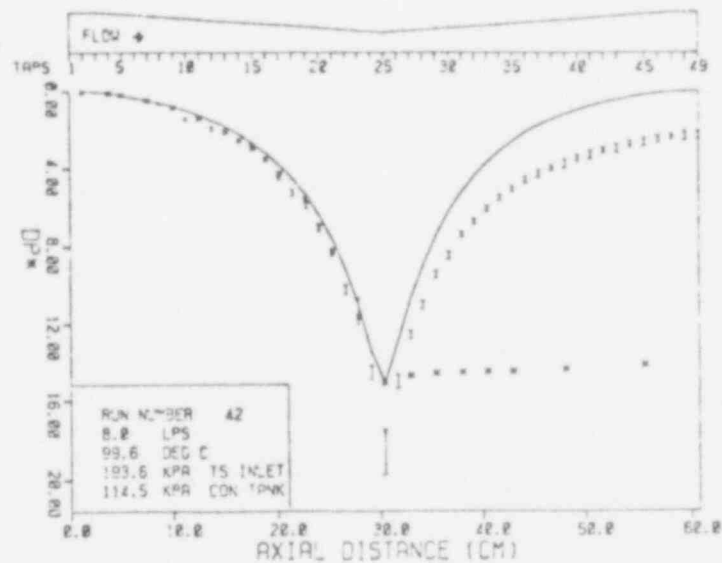
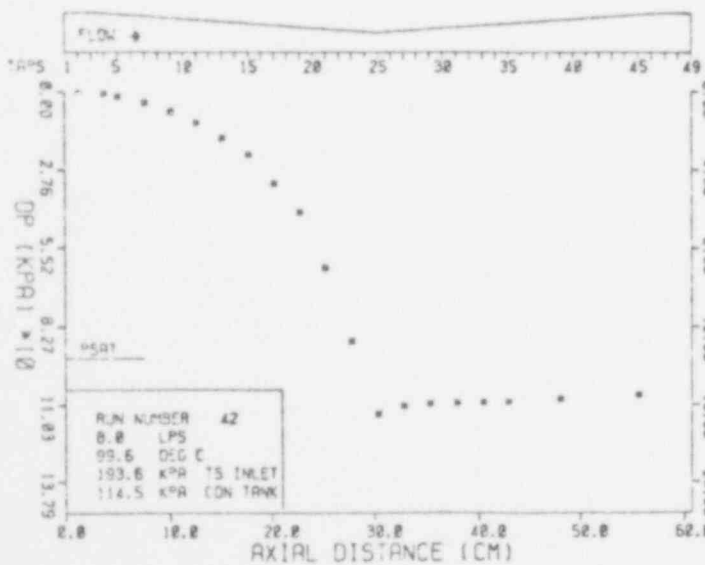


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 42

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	.28	.04
1-4	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	.75	.10
1-5	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	1.65	.22
1-7	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	3.66	.49
1-9	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	6.56	.87
1-11	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	10.76	1.43
1-13	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	16.06	2.14
1-15	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	21.93	2.92
1-17	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	32.27	4.29
1-19	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	42.47	5.65
1-21	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	61.92	8.23
1-23	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	87.70	11.66
1-25	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	113.49	15.09
1-27	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	110.73	14.72
1-29	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	109.83	14.61
1-31	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	109.42	14.55
1-33	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	109.21	14.51
1-35	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	109.01	14.50
1-39	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	107.37	14.36
1-45	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	106.59	14.17
1-49	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	104.66	13.92
50-1	8.01	95.7	99.6	99.4	193.6	114.5	394.5	.671E+06	6.34	.84

POOR ORIGINAL

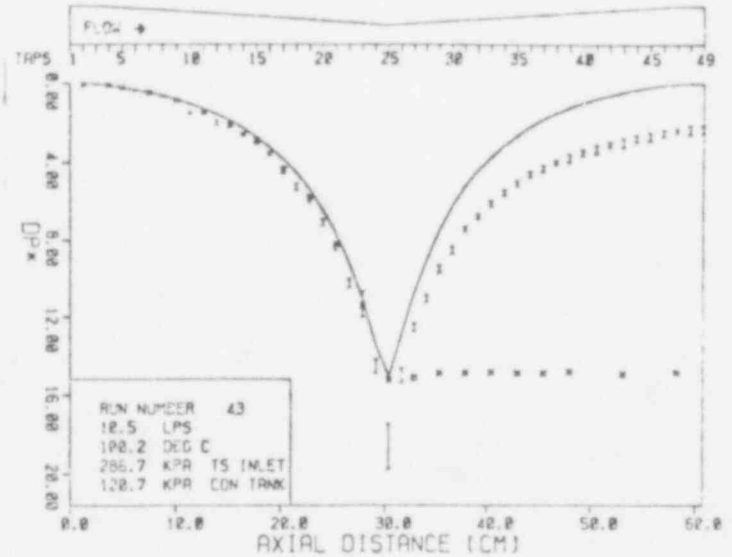
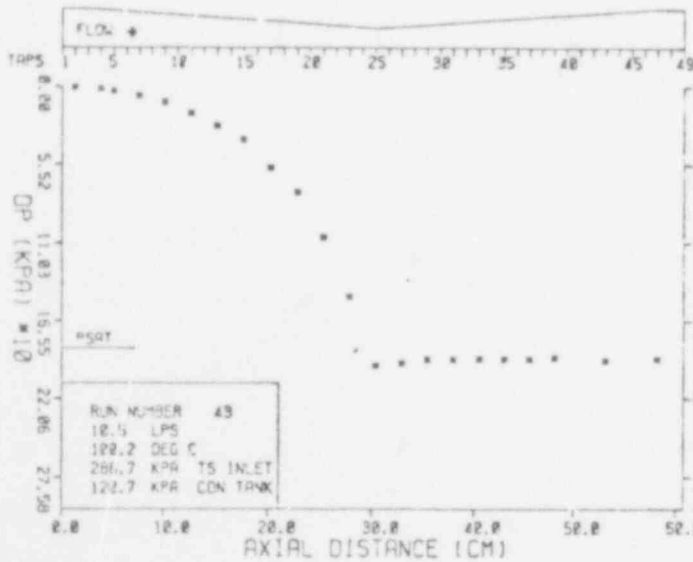


BML FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 43

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	.47	.04
1-4	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	1.40	.11
1-5	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	2.90	.22
1-7	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	6.39	.49
1-9	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	11.10	.86
1-11	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	18.82	1.46
1-17	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	27.44	2.12
1-15	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	37.09	2.87
1-17	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	57.23	4.42
1-19	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	74.81	5.78
1-21	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	106.04	8.20
1-23	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	147.82	11.43
1-25	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	197.19	15.24
1-27	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	255.54	19.12
1-29	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	322.78	24.90
1-31	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	392.50	31.89
1-33	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	462.23	38.86
1-35	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	532.85	44.91
1-37	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	602.78	49.90
1-39	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	671.74	54.82
1-43	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	733.47	59.96
1-47	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	782.50	64.43
1-49	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	822.09	68.55
50-1	10.51	97.2	100.2	99.9	286.7	120.7	517.6	.884E+06	860.00	72.00

POOR ORIGINAL



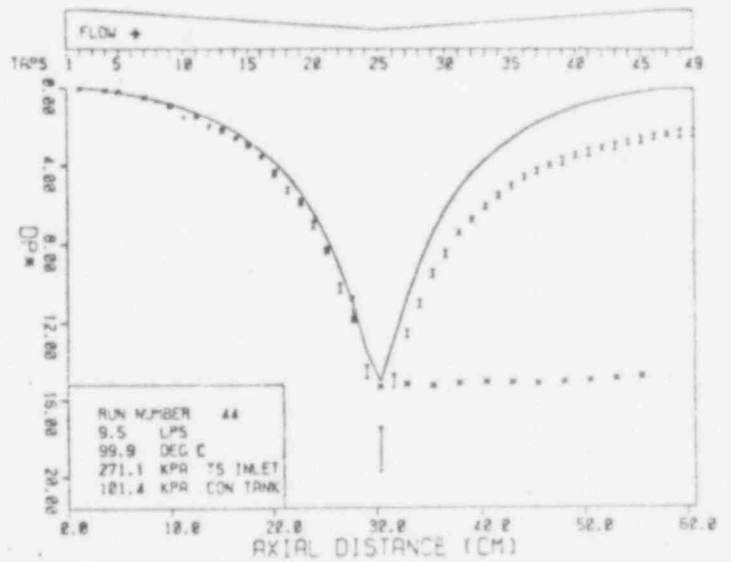
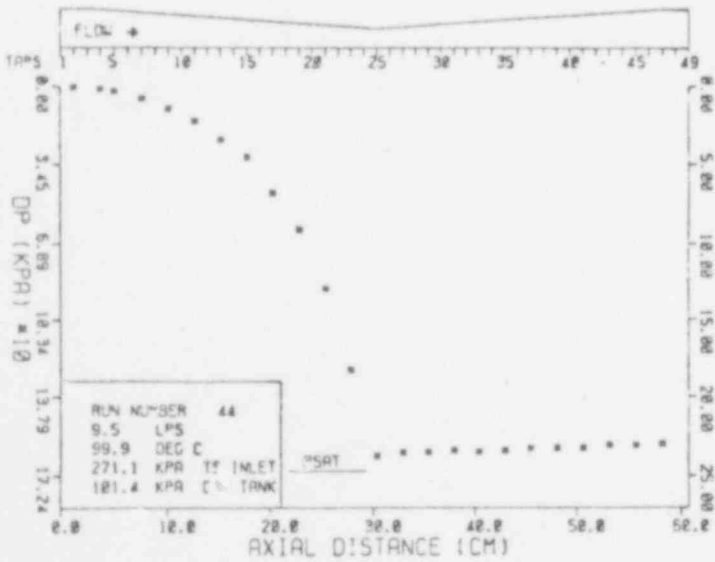
575 165

BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 44

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	9.53	97.0	99.9	99.9	271.1	101.4	469.0	.799E+06	.38	.04
1-4	9.53	97.0	99.9	99.9	271.1	101.4	469.3	.799E+06	1.07	.10
1-5	9.53	97.0	99.9	99.9	271.1	101.4	469.1	.799E+06	1.99	.19
1-7	9.52	97.0	99.9	99.9	271.1	101.4	469.0	.799E+06	5.24	.49
1-9	9.51	97.0	99.9	99.9	271.1	101.4	468.3	.799E+06	9.74	.97
1-11	9.54	97.0	99.9	99.9	271.1	101.4	469.7	.800E+06	15.51	1.36
1-13	9.54	97.0	99.9	99.9	271.1	101.4	469.6	.800E+06	23.62	2.22
1-15	9.56	97.0	99.9	99.9	271.1	101.4	470.7	.802E+06	31.14	2.91
1-17	9.58	97.0	99.9	99.9	271.1	101.4	471.6	.803E+06	46.84	4.36
1-19	9.56	97.0	99.9	99.9	271.1	101.4	470.7	.802E+06	62.92	5.88
1-21	9.53	97.0	99.9	99.9	271.1	101.4	469.3	.799E+06	80.14	7.38
1-23	9.52	97.0	99.9	99.9	271.1	101.4	468.8	.799E+06	125.82	11.65
1-25	9.55	97.0	99.9	99.9	271.1	101.4	470.2	.801E+06	162.56	15.31
1-27	9.55	97.0	99.9	99.9	271.1	101.4	470.3	.801E+06	182.19	17.18
1-29	9.52	97.0	99.9	99.9	271.1	101.4	468.9	.799E+06	161.96	15.25
1-31	9.54	97.0	99.9	99.9	271.1	101.4	469.9	.800E+06	161.35	15.13
1-33	9.53	97.0	99.9	99.9	271.1	101.4	471.6	.803E+06	161.97	15.08
1-35	9.56	97.0	99.9	99.9	271.1	101.4	470.7	.802E+06	161.38	15.04
1-37	9.52	97.0	99.9	99.9	271.1	101.4	468.8	.799E+06	160.47	15.12
1-39	9.53	97.0	99.9	99.9	271.1	101.4	469.5	.800E+06	160.36	15.06
1-41	9.55	97.0	99.9	99.9	271.1	101.4	470.3	.801E+06	160.29	15.00
1-43	9.54	97.0	99.9	99.9	271.1	101.4	469.9	.800E+06	158.87	14.80
1-45	9.52	97.0	99.9	99.9	271.1	101.4	471.4	.803E+06	158.96	14.81
1-47	9.52	97.0	99.9	99.9	271.1	101.4	468.6	.799E+06	158.32	14.93
1-49	9.54	97.0	99.9	99.9	271.1	101.4	469.9	.800E+06	157.55	14.77
50-1	9.54	97.0	99.9	100.0	271.1	101.4	469.7	.800E+06	15.02	1.41

POOR ORIGINAL

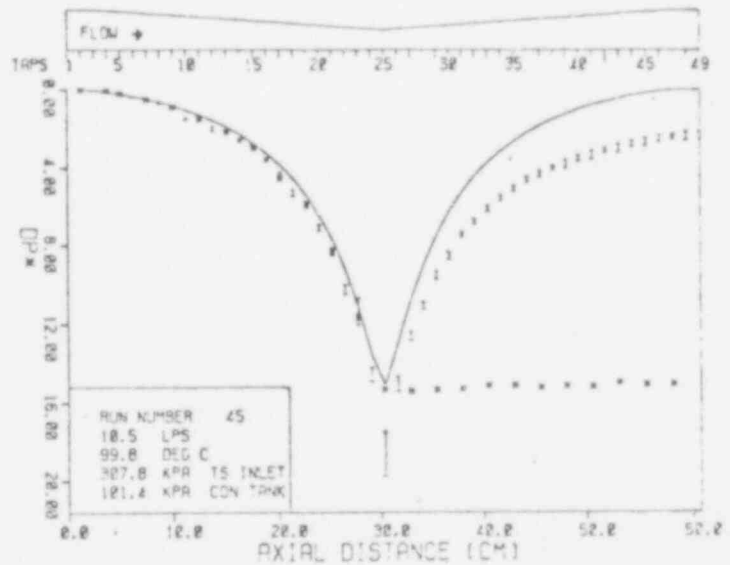
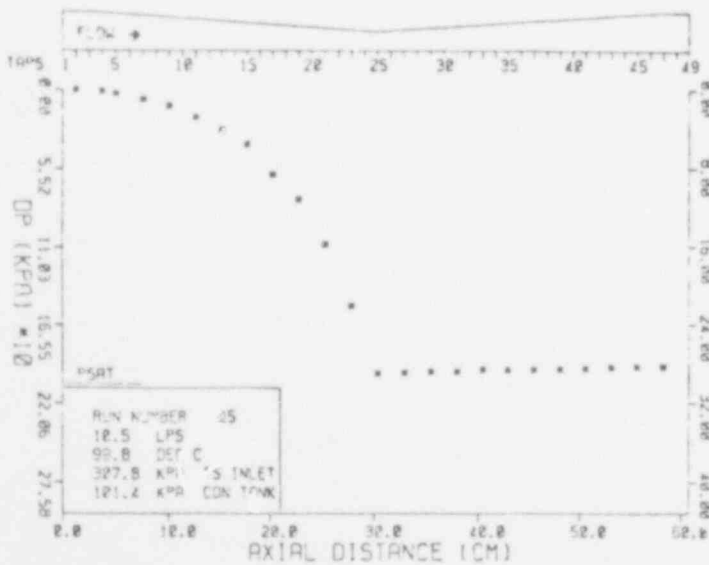


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 45

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	10.52	97.5	100.1	100.1	307.8	101.4	518.0	.884E+06	.13	.01
1-4	10.51	97.5	100.1	100.1	307.8	101.4	517.6	.883E+06	.91	.07
1-5	10.55	97.5	100.1	100.1	307.8	101.4	519.3	.886E+06	2.59	.20
1-7	10.54	97.5	100.1	100.1	307.8	101.4	518.8	.886E+06	6.58	.51
1-9	10.53	97.5	100.0	100.1	307.8	101.4	518.7	.885E+06	11.41	.89
1-11	10.50	97.5	100.0	100.1	307.8	101.4	517.1	.882E+06	19.39	1.50
1-13	10.51	97.5	100.1	100.1	307.8	101.4	517.6	.883E+06	27.78	2.15
1-15	10.52	97.5	100.0	100.0	307.8	101.4	518.0	.883E+06	37.71	2.91
1-17	10.50	97.4	100.0	100.0	307.8	101.4	517.2	.882E+06	58.70	4.54
1-19	10.55	97.4	99.9	100.0	307.8	101.4	519.5	.885E+06	76.11	5.84
1-21	10.53	97.4	99.9	100.0	307.8	101.4	518.5	.884E+06	107.99	8.32
1-23	10.55	97.4	99.9	100.0	307.8	101.4	519.3	.885E+06	151.76	11.65
1-25	10.55	97.4	99.9	100.0	307.8	101.4	519.4	.885E+06	199.38	15.30
1-27	10.50	97.4	99.9	99.9	307.8	101.4	517.2	.882E+06	146.83	11.39
1-29	10.51	97.3	99.9	99.9	307.8	101.4	517.4	.882E+06	157.91	12.30
1-31	10.52	97.3	99.9	99.9	307.8	101.4	517.9	.882E+06	198.04	15.29
1-33	10.54	97.3	99.8	99.9	307.8	101.4	518.9	.884E+06	196.72	15.12
1-35	10.55	97.3	99.8	99.9	307.8	101.4	519.6	.885E+06	197.02	15.11
1-37	10.51	97.3	99.8	99.9	307.8	101.4	517.6	.882E+06	196.64	15.10
1-39	10.53	97.3	99.8	99.9	307.8	101.4	518.3	.882E+06	196.14	15.12
1-41	10.50	97.3	99.8	99.9	307.8	101.4	517.1	.882E+06	195.69	15.15
1-43	10.55	97.3	99.8	99.9	307.8	101.4	519.6	.885E+06	195.00	14.95
1-45	10.51	97.3	99.8	99.9	307.8	101.4	517.4	.882E+06	194.79	15.06
1-47	10.52	97.3	99.8	99.9	307.8	101.4	518.2	.882E+06	194.69	15.01
1-49	10.55	97.3	99.8	99.9	307.8	101.4	519.4	.884E+06	194.14	14.90
50-1	10.54	97.3	99.8	99.9	307.8	101.4	519.0	.884E+06	18.34	1.41

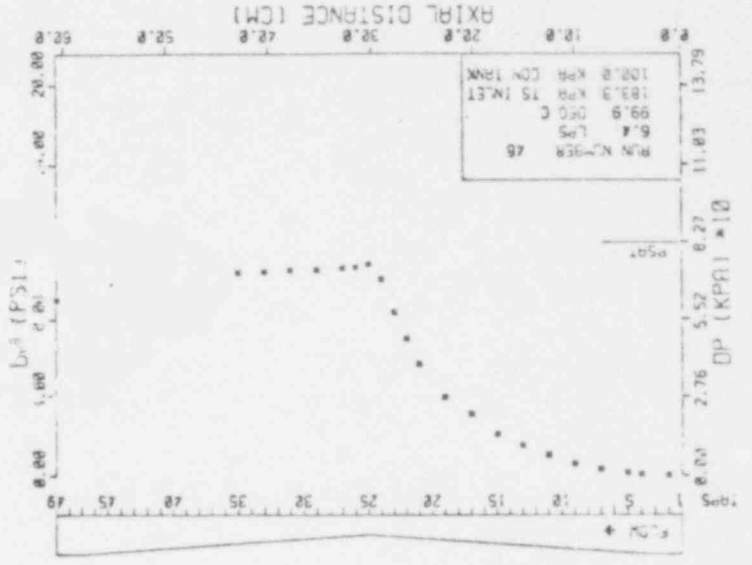
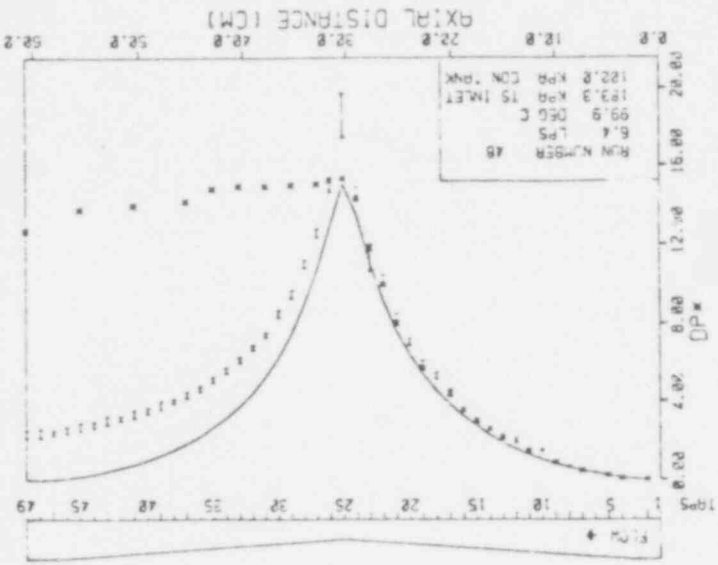
POOR ORIGINAL





575 169

-137-



POOR ORIGINAL

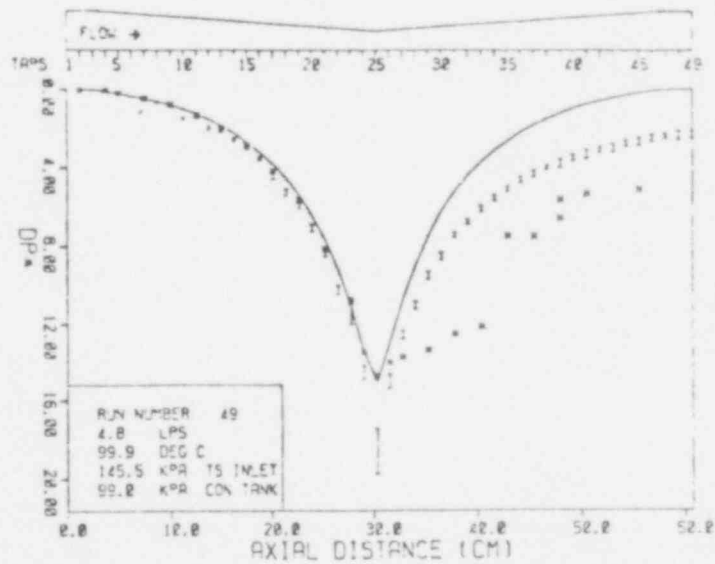
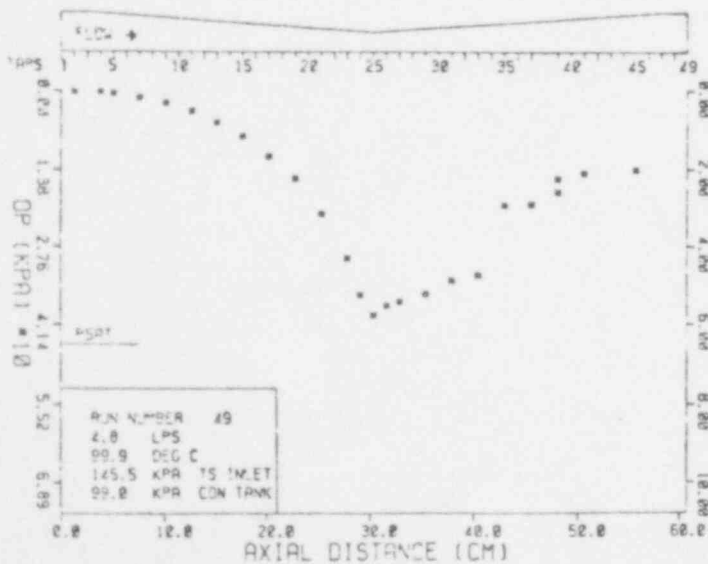
LOOP FLOW	TEMPERATURES (DEG C)	PRESSURE (KPA)	VELOCITY	REYNOLDS	DIFFERENTIAL PRESSURE
LIT/SEC	FLOW METER TS INLET COND TANK TS INLET COND TANK	TS INLET COND TANK	CM SEC	NUMBER	MEASURED DIMENSIONLESS
1-2	6.43	99.7	183.3	316.7	.02
1-4	6.44	99.8	183.3	317.0	.08
1-5	6.44	99.8	183.3	315.9	.24
1-7	6.42	99.8	183.3	317.1	.48
1-9	6.44	99.8	183.3	317.5	.88
1-11	6.45	99.8	183.3	316.5	1.47
1-13	6.43	99.8	183.3	317.4	2.17
1-15	6.45	99.8	183.3	317.4	2.96
1-17	6.45	99.8	183.3	317.8	4.41
1-19	6.42	99.8	183.3	316.1	5.70
1-21	6.45	99.9	183.3	317.8	8.03
1-23	6.44	99.9	183.3	315.7	10.00
1-25	6.42	99.9	183.3	317.3	11.81
1-27	6.45	99.9	183.3	316.1	14.35
1-29	6.42	99.9	183.3	317.6	15.24
1-31	6.44	99.9	183.3	317.6	15.34
1-33	6.42	99.9	183.3	315.9	15.05
1-35	6.44	99.9	183.3	317.7	15.02
1-37	6.47	99.9	183.3	317.7	14.96
1-39	6.47	99.9	183.3	316.9	14.82
1-41	6.47	99.9	183.3	318.4	14.17
1-43	6.43	99.9	183.3	318.7	13.98
1-45	6.47	99.9	183.3	318.8	13.79
1-47	6.47	99.9	183.3	316.8	13.29
50-1	6.43	99.3	183.3	316.5	1.31

BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 49

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	4.80	93.0	99.4	99.3	145.5	99.0	236.3	.401E+06	.12	.04
1-4	4.79	93.1	99.6	99.4	145.5	99.0	236.0	.401E+06	.18	.07
1-5	4.80	93.1	99.7	99.4	145.5	99.0	236.5	.402E+06	.51	.19
1-7	4.81	93.2	99.6	99.5	145.5	99.0	236.7	.402E+06	1.22	.45
1-9	4.79	93.2	99.8	99.5	145.5	99.0	235.9	.402E+06	2.11	.79
1-11	4.78	93.2	99.5	99.6	145.5	99.0	235.5	.400E+06	3.49	1.30
1-13	4.80	93.3	99.5	99.6	145.5	99.0	236.5	.402E+06	5.42	2.01
1-15	4.78	93.3	99.7	99.6	145.5	99.0	235.5	.401E+06	7.77	2.90
1-17	4.81	93.3	99.8	99.6	145.5	99.0	236.8	.403E+06	11.37	4.20
1-19	4.80	93.4	99.8	99.7	145.5	99.0	236.4	.403E+06	15.28	5.66
1-21	4.76	93.4	99.9	99.7	145.5	99.0	234.5	.400E+06	21.55	8.12
1-23	4.83	93.4	99.8	99.7	145.5	99.0	237.6	.405E+06	29.63	10.86
1-24	4.79	93.5	99.7	99.8	145.5	99.0	235.9	.401E+06	36.22	13.48
1-25	4.80	93.5	99.9	99.8	145.5	99.0	236.3	.403E+06	39.69	14.72
1-26	4.81	93.5	100.2	99.8	145.5	99.0	236.8	.405E+06	37.98	14.03
1-27	4.82	93.5	99.8	99.8	145.5	99.0	237.3	.404E+06	37.39	13.74
1-29	4.80	93.5	99.9	99.9	145.5	99.0	236.6	.403E+06	36.09	13.35
1-31	4.79	93.5	99.9	99.9	145.5	99.0	235.8	.402E+06	33.64	12.52
1-33	4.80	93.6	99.9	99.8	145.5	99.0	236.3	.403E+06	32.68	12.12
1-35	4.80	93.6	99.9	99.9	145.5	99.0	236.2	.403E+06	29.19	9.46
1-37	4.77	93.6	99.9	99.9	145.5	99.0	234.8	.400E+06	19.94	7.49
1-39	4.83	93.6	99.9	99.9	145.5	99.0	237.7	.405E+06	15.36	5.63
1-39	4.80	93.6	99.9	99.9	145.5	99.0	236.5	.403E+06	17.73	6.57
1-41	4.80	93.6	99.9	99.9	145.5	99.0	236.3	.403E+06	14.43	5.35
1-45	4.80	93.6	99.8	99.9	145.5	99.0	236.4	.403E+06	13.83	5.12
1-49	4.78	93.6	99.9	99.9	145.5	99.0	235.2	.401E+06	10.81	4.04
50-1	4.79	93.6	99.9	99.9	145.5	99.0	235.8	.402E+06	2.78	1.04

POOR ORIGINAL



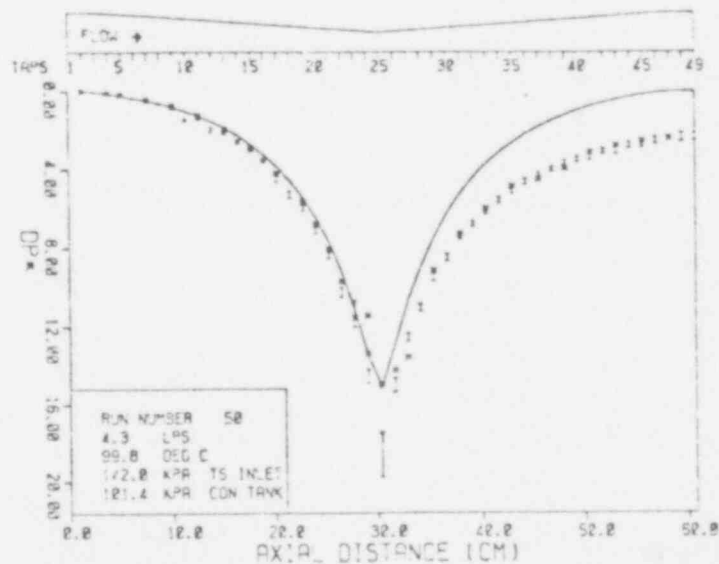
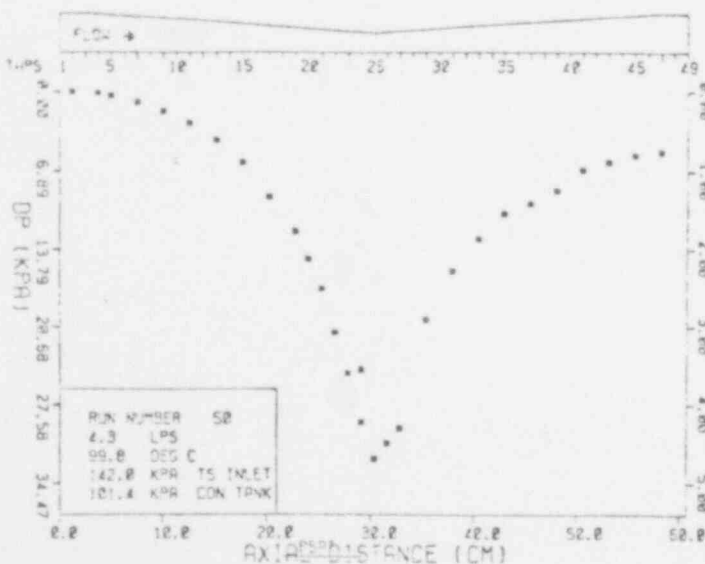


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 50

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	4.31	92.8	99.9	99.9	142.0	101.4	212.3	.362E+06	.00	.00
1-4	4.28	92.8	100.2	99.9	142.0	101.4	210.6	.360E+06	.14	.06
1-5	4.31	92.8	100.0	99.9	142.0	101.4	212.3	.362E+06	.36	.17
1-7	4.29	92.9	99.9	99.9	142.0	101.4	211.1	.360E+06	.93	.43
1-9	4.32	92.8	100.0	99.9	142.0	101.4	212.8	.363E+06	1.67	.76
1-11	4.33	92.8	100.1	99.9	142.0	101.4	213.3	.364E+06	2.74	1.25
1-13	4.33	92.8	99.9	99.9	142.0	101.4	213.4	.364E+06	4.20	1.91
1-15	4.29	92.8	100.1	99.9	142.0	101.4	211.0	.360E+06	6.14	2.85
1-17	4.31	92.8	99.9	99.9	142.0	101.4	212.2	.362E+06	9.15	4.21
1-19	4.29	92.8	99.9	99.9	142.0	101.4	211.3	.360E+06	12.22	5.66
1-20	4.30	92.8	100.1	99.9	142.0	101.4	211.6	.361E+06	14.62	6.76
1-21	4.29	92.8	100.0	99.9	142.0	101.4	211.0	.360E+06	17.27	8.03
1-22	4.32	92.8	99.9	99.9	142.0	101.4	212.9	.363E+06	21.21	9.69
1-23	4.28	92.8	100.0	99.9	142.0	101.4	211.0	.360E+06	24.82	11.54
1-24	4.28	92.8	100.0	99.9	142.0	101.4	210.6	.359E+06	24.47	11.42
1-25	4.29	92.8	100.0	99.9	142.0	101.4	211.0	.360E+06	32.34	15.04
1-24	4.31	92.8	99.9	99.9	142.0	101.4	212.4	.362E+06	29.13	13.36
1-26	4.31	92.8	100.1	99.9	142.0	101.4	212.3	.362E+06	30.97	14.23
1-27	4.32	92.8	99.9	99.9	142.0	101.4	212.6	.362E+06	29.64	13.57
1-29	4.32	92.8	99.8	99.9	142.0	101.4	212.5	.362E+06	20.02	9.17
1-31	4.29	92.8	100.0	99.9	142.0	101.4	211.5	.361E+06	15.73	7.28
1-33	4.28	92.8	99.8	99.9	142.0	101.4	210.6	.359E+06	12.85	6.00
1-35	4.31	92.8	99.9	99.9	142.0	101.4	212.5	.362E+06	10.61	4.87
1-37	4.30	92.7	99.9	99.9	142.0	101.4	211.8	.361E+06	9.73	4.49
1-39	4.31	92.8	100.0	99.9	142.0	101.4	212.0	.362E+06	8.57	3.95
1-41	4.29	92.7	100.0	99.9	142.0	101.4	211.3	.361E+06	6.76	3.14
1-43	4.30	92.7	100.0	99.8	142.0	101.4	211.9	.362E+06	6.07	2.80
1-45	4.29	92.7	99.9	99.8	142.0	101.4	211.1	.360E+06	5.52	2.57
1-47	4.31	92.7	99.8	99.8	142.0	101.4	212.4	.362E+06	5.22	2.39
1-49	4.29	92.7	100.2	99.9	142.0	101.4	211.4	.361E+06	4.63	2.15
50-1	4.29	92.8	99.8	99.9	142.0	101.4	211.1	.359E+06	2.05	.95

POOR ORIGINAL

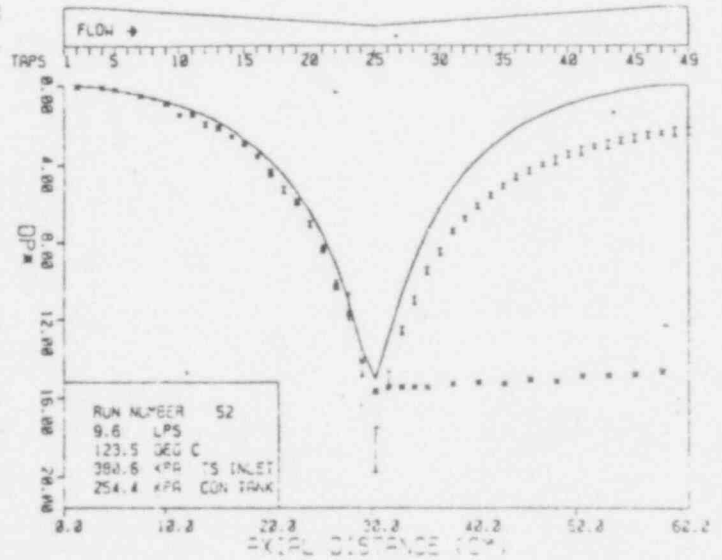
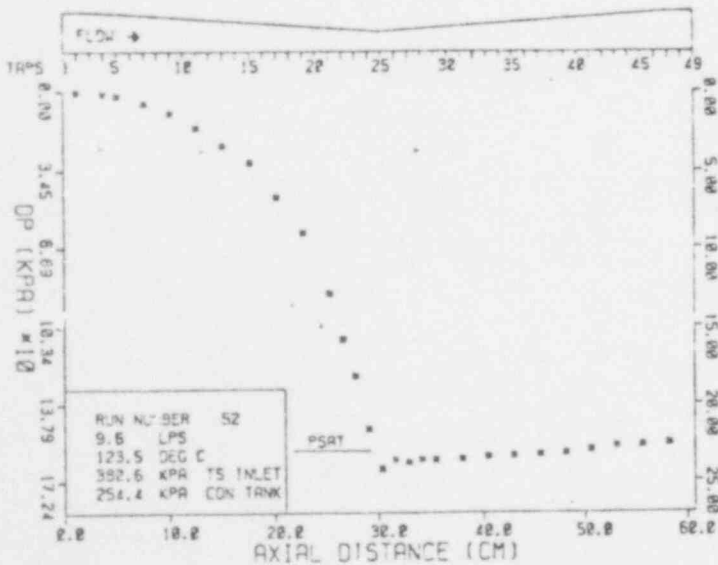


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 52

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM/SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	9.58	116.6	123.5	123.5	380.6	254.4	471.8	.982E+06	.48	.05
1-4	9.61	116.6	123.5	123.6	380.6	254.4	473.3	.985E+06	1.13	.11
1-5	9.56	116.6	123.5	123.6	380.6	254.4	471.0	.980E+06	2.15	.20
1-7	9.61	116.6	123.5	123.5	380.6	254.4	473.2	.985E+06	5.33	.50
1-9	9.59	116.6	123.5	123.5	380.6	254.4	472.1	.982E+06	9.42	.89
1-11	9.60	116.6	123.5	123.5	380.6	254.4	473.0	.984E+06	15.77	1.49
1-13	9.61	116.5	123.5	123.5	380.6	254.4	473.2	.985E+06	23.18	2.18
1-15	9.60	116.5	123.5	123.5	380.6	254.4	472.5	.983E+06	30.63	2.59
1-17	9.61	116.5	123.5	123.5	380.6	254.4	473.1	.984E+06	46.16	4.35
1-19	9.60	116.5	123.5	123.5	380.6	254.4	472.7	.984E+06	62.28	5.88
1-21	9.58	116.5	123.5	123.5	380.6	254.4	471.9	.982E+06	88.77	8.41
1-22	9.59	116.6	123.5	123.5	380.6	254.4	472.0	.982E+06	108.93	10.32
1-23	9.64	116.6	123.5	123.5	380.6	254.4	474.7	.988E+06	125.22	11.72
1-24	9.58	116.5	123.5	123.5	380.6	254.4	471.9	.982E+06	148.92	14.11
1-25	9.63	116.6	123.5	123.5	380.6	254.4	474.2	.987E+06	166.77	15.65
1-26	9.58	116.6	123.5	123.5	380.6	254.4	471.6	.981E+06	162.88	15.45
1-27	9.61	116.6	123.5	123.5	380.6	254.4	473.3	.985E+06	163.84	15.44
1-28	9.58	116.6	123.5	123.5	380.6	254.4	471.6	.982E+06	162.66	15.43
1-29	9.58	116.6	123.5	123.5	380.6	254.4	471.8	.982E+06	162.92	15.45
1-31	9.62	116.5	123.5	123.5	380.6	254.4	473.8	.986E+06	162.51	15.28
1-33	9.61	116.6	123.6	123.5	380.6	254.4	473.2	.985E+06	161.27	15.20
1-35	9.58	116.6	123.5	123.5	380.6	254.4	471.9	.982E+06	161.02	15.26
1-37	9.63	116.6	123.6	123.6	380.6	254.4	474.0	.987E+06	160.47	15.17
1-39	9.59	116.6	123.6	123.6	380.6	254.4	472.2	.983E+06	159.96	15.14
1-41	9.63	116.6	123.5	123.6	380.6	254.4	474.0	.987E+06	158.41	14.88
1-43	9.59	116.6	123.5	123.6	380.6	254.4	472.4	.983E+06	156.86	14.83
1-45	9.60	116.6	123.6	123.6	380.6	254.4	472.7	.984E+06	156.52	14.78
1-47	9.62	116.6	123.5	123.5	380.6	254.4	473.5	.985E+06	155.64	14.65
1-49	9.60	116.6	123.5	123.5	380.6	254.4	472.7	.984E+06	154.62	14.60
1-50	9.63	116.6	123.5	123.5	380.6	254.4	474.1	.987E+06	15.18	1.42

POOR ORIGINAL

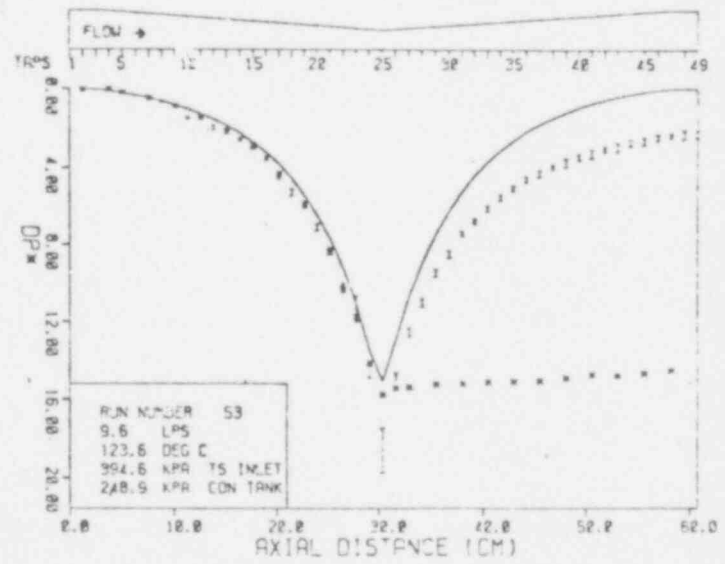
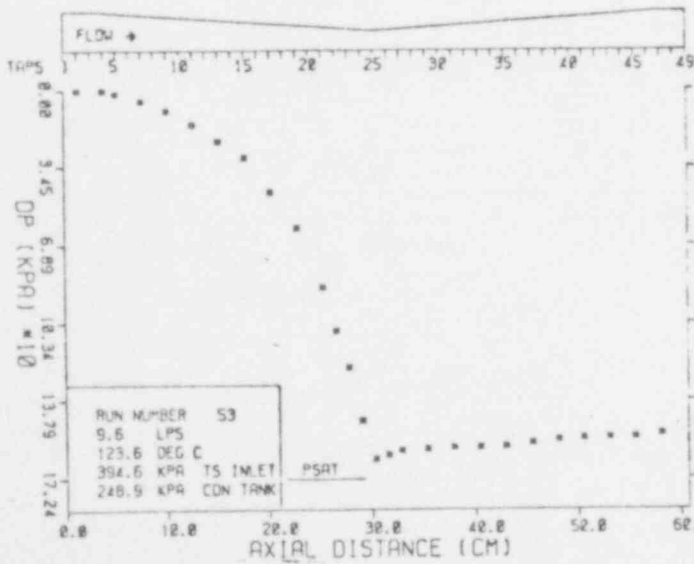


BNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER 53

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM/SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	9.55	116.6	123.5	123.6	394.6	248.9	478.3	.979E+06	.37	.03
1-4	9.55	116.6	123.5	123.6	394.6	248.9	478.3	.979E+06	.51	.05
1-5	9.50	116.6	123.5	123.6	394.6	248.9	468.0	.974E+06	1.98	.19
1-7	9.54	116.6	123.6	123.6	394.6	248.9	470.0	.978E+06	5.04	.48
1-9	9.58	116.6	123.6	123.6	394.6	248.9	471.6	.982E+06	9.23	.88
1-11	9.53	116.6	123.5	123.6	394.6	248.9	469.4	.977E+06	15.50	1.48
1-13	9.55	116.6	123.6	123.6	394.6	248.9	470.2	.979E+06	23.85	2.20
1-15	9.54	116.6	123.6	123.6	394.6	248.9	469.8	.978E+06	30.10	2.88
1-17	9.55	116.6	123.6	123.6	394.6	248.9	470.2	.979E+06	45.56	4.35
1-19	9.55	116.6	123.6	123.6	394.6	248.9	470.5	.979E+06	61.39	5.85
1-21	9.53	116.6	123.6	123.6	394.6	248.9	469.2	.977E+06	87.53	8.39
1-22	9.50	116.6	123.6	123.6	394.6	248.9	467.8	.974E+06	107.02	10.32
1-23	9.55	116.6	123.5	123.6	394.6	248.9	470.5	.979E+06	123.36	11.76
1-24	9.51	116.6	123.5	123.6	394.6	248.9	468.3	.975E+06	146.98	14.14
1-25	9.51	116.6	123.5	123.6	394.6	248.9	468.5	.975E+06	163.85	15.75
1-26	9.55	116.6	123.5	123.6	394.6	248.9	470.5	.979E+06	161.96	15.44
1-27	9.52	116.6	123.5	123.6	394.6	248.9	468.9	.976E+06	169.32	15.39
1-29	9.55	116.6	123.5	123.6	394.6	248.9	470.2	.979E+06	159.61	15.23
1-31	9.53	116.6	123.5	123.6	394.6	248.9	469.5	.977E+06	158.99	15.22
1-33	9.56	116.6	123.5	123.6	394.6	248.9	470.7	.980E+06	158.78	15.12
1-35	9.56	116.6	123.5	123.6	394.6	248.9	470.7	.980E+06	158.37	15.08
1-37	9.53	116.6	123.5	123.6	394.6	248.9	469.4	.977E+06	157.10	15.05
1-39	9.54	116.6	123.5	123.6	394.6	248.9	469.6	.977E+06	155.70	14.90
1-41	9.56	116.6	123.6	123.6	394.6	248.9	470.7	.980E+06	154.84	14.75
1-43	9.53	116.6	123.6	123.6	394.6	248.9	469.4	.977E+06	154.59	14.81
1-45	9.56	116.6	123.6	123.6	394.6	248.9	471.0	.980E+06	154.34	14.68
1-47	9.56	116.6	123.6	123.6	394.6	248.9	470.9	.980E+06	152.91	14.55
1-49	9.53	116.6	123.5	123.6	394.6	248.9	469.5	.977E+06	152.38	14.59
50-1	9.56	116.6	123.6	123.6	394.6	248.9	470.9	.980E+06	14.94	1.42

POOR ORIGINAL



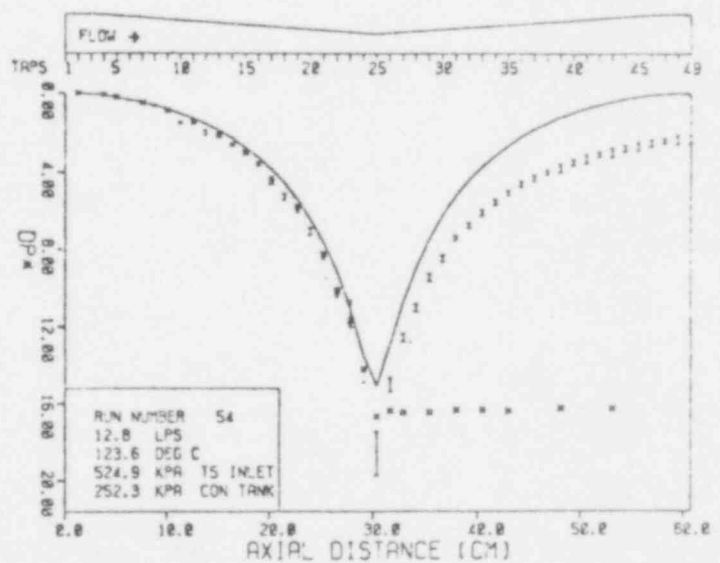
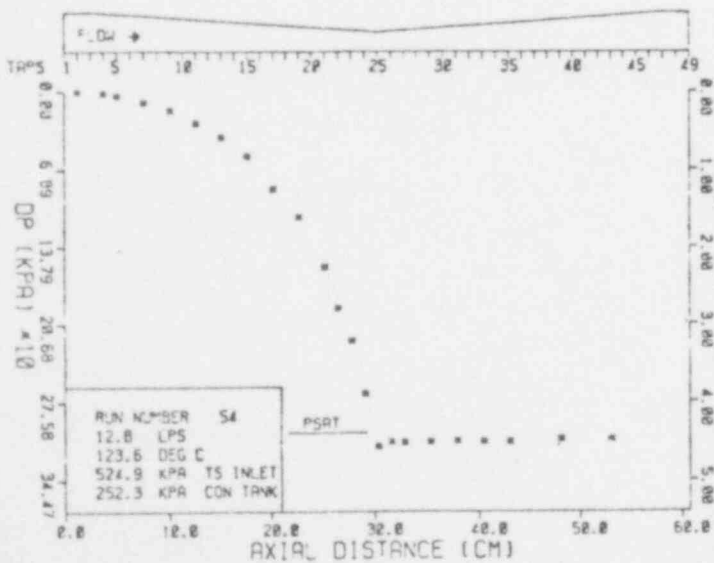
575 173

BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 54

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	12.85	118.4	123.5	123.6	524.9	252.3	632.5	.132E+07	.00	.00
1-4	12.83	118.5	123.6	123.7	524.9	252.3	631.9	.132E+07	1.51	.08
1-5	12.87	118.5	123.6	123.7	524.9	252.3	633.6	.132E+07	3.76	.20
1-7	12.86	118.6	123.7	123.8	524.9	252.3	633.2	.132E+07	9.50	.50
1-9	12.85	118.6	123.7	123.8	524.9	252.3	633.0	.132E+07	16.57	.87
1-11	12.84	118.6	123.7	123.8	524.9	252.3	632.4	.132E+07	27.51	1.45
1-13	12.81	118.6	123.7	123.8	524.9	252.3	630.7	.131E+07	39.92	2.12
1-15	12.84	118.6	123.6	123.7	524.9	252.3	632.0	.132E+07	56.76	3.00
1-17	12.85	118.6	123.6	123.7	524.9	252.3	632.9	.132E+07	85.53	4.51
1-19	12.87	118.6	123.6	123.7	524.9	252.3	633.9	.132E+07	110.25	5.79
1-21	12.82	118.6	123.6	123.7	524.9	252.3	631.2	.131E+07	155.62	8.24
1-22	12.82	118.6	123.6	123.7	524.9	252.3	631.5	.131E+07	192.43	10.18
1-23	12.84	118.6	123.6	123.7	524.9	252.3	632.2	.132E+07	221.48	11.69
1-24	12.82	118.6	123.6	123.7	524.9	252.3	631.1	.131E+07	267.75	14.18
1-25	12.82	118.6	123.6	123.7	524.9	252.3	631.4	.131E+07	314.88	16.66
1-26	12.85	118.6	123.6	123.7	524.9	252.3	632.8	.132E+07	310.94	16.39
1-27	12.83	118.6	123.6	123.7	524.9	252.3	631.9	.132E+07	311.36	16.45
1-29	12.83	118.6	123.6	123.7	524.9	252.3	631.9	.132E+07	311.38	16.45
1-31	12.86	118.6	123.6	123.7	524.9	252.3	633.1	.132E+07	310.17	16.33
1-33	12.87	118.6	123.6	123.7	524.9	252.3	633.7	.132E+07	310.56	16.31
1-35	12.85	118.6	123.6	123.6	524.9	252.3	632.6	.132E+07	310.59	16.37
1-39	12.86	118.6	123.6	123.6	524.9	252.3	633.1	.132E+07	308.51	16.24
1-43	12.83	118.6	123.6	123.6	524.9	252.3	631.9	.131E+07	307.81	16.27
1-49	12.84	118.6	123.6	123.6	524.9	252.3	632.2	.132E+07	306.33	16.17
50-1	12.81	118.5	123.6	123.6	524.9	252.3	631.0	.131E+07	28.05	1.49

POOR ORIGINAL

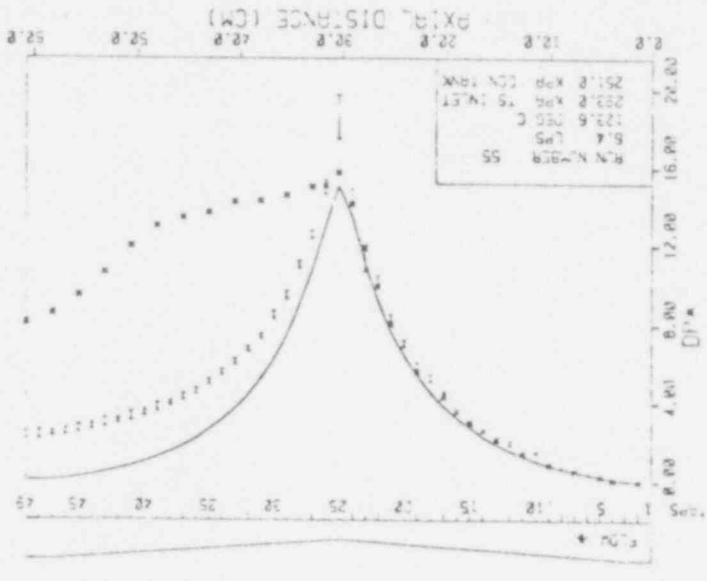
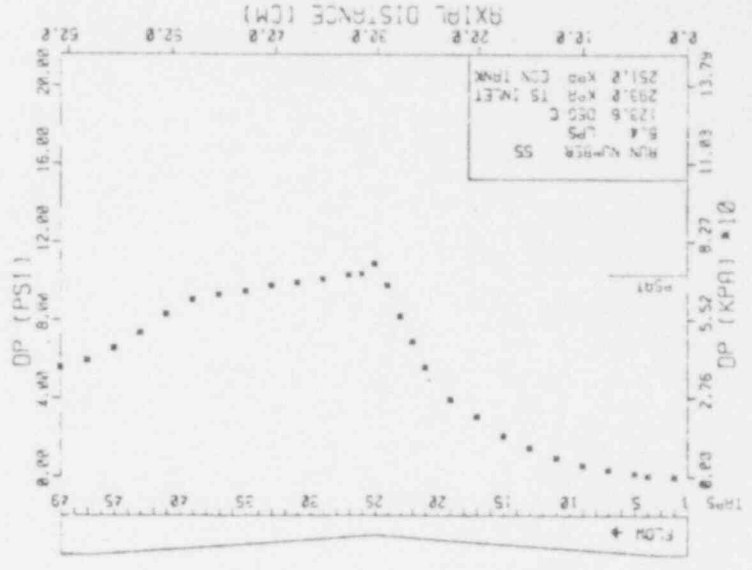


BNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER 55

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)	PRESSURE (KPA)	TS INLET COND TANK	TS INLET COND TANK	VELOCITY CM/SEC	REYNOLDS NUMBER	MEASURED DIFFERENTIAL PRESSURE DIMENSIONLESS
1-2	6.45	110.4	120.8	251.0	251.0	317.4	6623+06	0.01
1-4	6.42	110.4	120.6	251.0	251.0	316.0	6588+06	0.08
1-5	6.46	110.4	120.6	251.0	251.0	317.9	6623+06	0.24
1-7	6.47	110.4	120.6	251.0	251.0	316.4	6598+06	0.52
1-9	6.44	110.4	120.6	251.0	251.0	317.2	6618+06	0.86
1-11	6.45	110.4	120.6	251.0	251.0	317.6	6623+06	1.42
1-13	6.46	110.3	120.6	251.0	251.0	318.0	6623+06	2.11
1-15	6.41	110.3	120.6	251.0	251.0	315.7	6572+06	3.00
1-17	6.49	110.2	120.6	251.0	251.0	319.4	6652+06	4.37
1-19	6.47	110.2	120.5	251.0	251.0	318.5	6623+06	5.58
1-21	6.44	110.2	120.5	251.0	251.0	317.3	6608+06	8.04
1-23	6.45	110.2	120.5	251.0	251.0	317.7	6618+06	9.91
1-25	6.46	110.2	120.5	251.0	251.0	317.0	6608+06	11.67
1-27	6.43	110.1	120.5	251.0	251.0	317.9	6623+06	14.09
1-29	6.41	110.1	120.5	251.0	251.0	316.4	6598+06	15.05
1-31	6.46	110.1	120.5	251.0	251.0	317.8	6618+06	15.94
1-33	6.43	110.1	120.5	251.0	251.0	318.1	6623+06	16.25
1-35	6.43	110.1	120.6	251.0	251.0	316.4	6598+06	16.27
1-37	6.45	110.2	120.6	251.0	251.0	317.7	6623+06	16.46
1-39	6.45	110.2	120.6	251.0	251.0	317.7	6623+06	16.46
1-41	6.44	110.2	120.6	251.0	251.0	317.3	6608+06	16.44
1-43	6.43	110.2	120.6	251.0	251.0	317.8	6623+06	16.44
1-45	6.43	110.2	120.6	251.0	251.0	317.3	6608+06	16.44
1-47	6.43	110.2	120.6	251.0	251.0	317.7	6623+06	16.44
1-49	6.43	110.2	120.6	251.0	251.0	317.6	6623+06	16.44
1-51	6.44	110.2	120.6	251.0	251.0	317.6	6623+06	16.44

**POOR ORIGINAL**

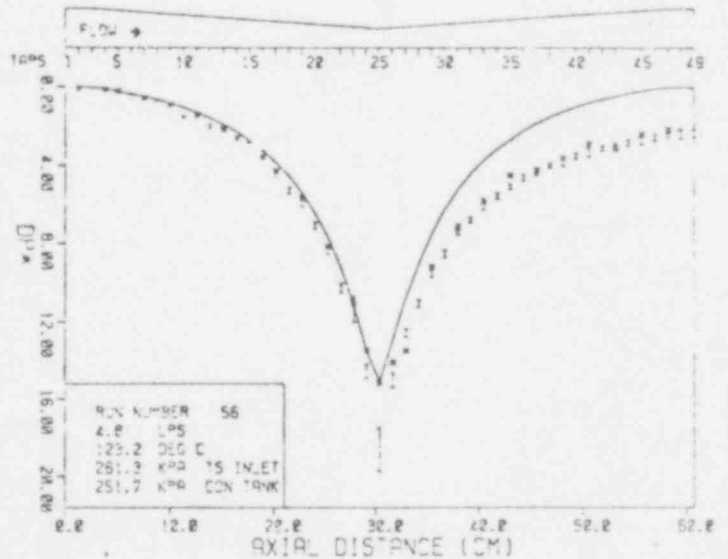
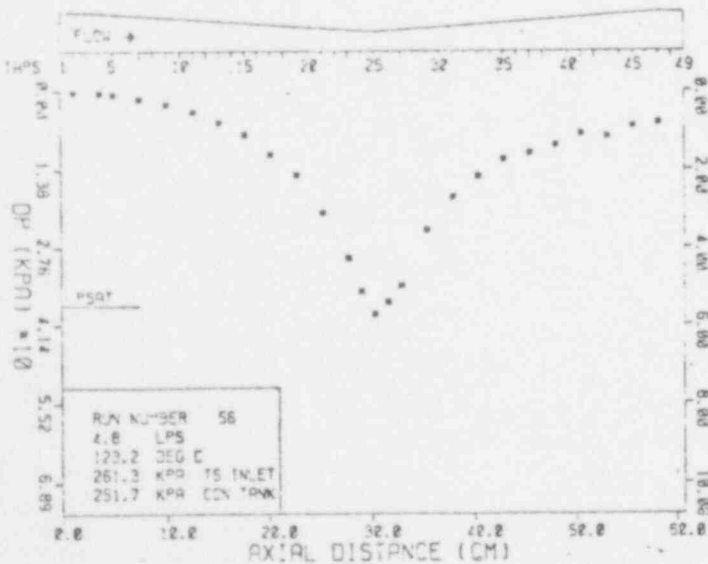


BNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER 56

TAPS	LOOP FLOW (TR/SEC)	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM/SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	4.75	109.4	123.5	123.4	261.3	251.7	233.7	.486E+06	.22	.09
1-4	4.79	109.5	123.6	123.5	261.3	251.7	235.7	.491E+06	.36	.14
1-5	4.76	109.6	124.0	123.6	261.3	251.7	234.6	.490E+06	.59	.23
1-7	4.75	109.6	124.2	123.6	261.3	251.7	233.8	.489E+06	1.44	.56
1-9	4.76	109.6	123.5	123.5	261.3	251.7	234.3	.488E+06	2.35	.90
1-11	4.81	109.6	123.3	123.4	261.3	251.7	236.9	.492E+06	3.07	1.38
1-13	4.75	109.5	123.9	123.6	261.3	251.7	233.7	.488E+06	5.54	2.14
1-15	4.76	109.6	124.2	123.7	261.3	251.7	234.3	.490E+06	7.65	2.94
1-17	4.75	109.5	124.0	123.6	261.3	251.7	233.9	.489E+06	11.08	4.27
1-19	4.75	109.6	124.5	123.8	261.3	251.7	233.9	.491E+06	14.67	5.66
1-21	4.78	109.5	123.6	123.6	261.3	251.7	235.5	.490E+06	21.36	8.13
1-23	4.81	109.5	123.6	123.6	261.3	251.7	237.0	.494E+06	29.38	11.04
1-24	4.78	109.6	123.9	123.7	261.3	251.7	235.5	.492E+06	35.32	13.44
1-25	4.76	109.6	123.7	123.6	261.3	251.7	234.4	.489E+06	39.43	15.15
1-26	4.80	109.6	124.0	123.7	261.3	251.7	236.5	.494E+06	37.32	14.09
1-27	4.71	109.6	123.5	123.6	261.3	251.7	232.0	.483E+06	34.40	13.48
1-29	4.83	109.6	123.7	123.7	261.3	251.7	237.8	.496E+06	24.56	9.16
1-31	4.78	109.6	124.2	123.7	261.3	251.7	235.6	.493E+06	18.69	7.11
1-33	4.75	109.6	124.2	123.7	261.3	251.7	233.9	.489E+06	15.03	5.80
1-35	4.83	109.6	123.9	123.7	261.3	251.7	237.8	.496E+06	12.08	4.51
1-37	4.75	109.6	123.8	123.7	261.3	251.7	234.0	.488E+06	10.91	4.20
1-39	4.79	109.6	124.0	123.7	261.3	251.7	235.8	.493E+06	9.48	3.74
1-41	4.76	109.6	123.2	123.5	261.3	251.7	234.6	.487E+06	7.49	2.87
1-43	4.79	109.5	123.2	123.5	261.3	251.7	235.7	.490E+06	8.02	3.04
1-45	4.76	109.5	123.5	123.6	261.3	251.7	234.4	.488E+06	6.15	2.36
1-47	4.76	109.5	123.6	123.6	261.3	251.7	234.1	.488E+06	5.57	2.15
1-49	4.77	109.5	124.0	123.6	261.3	251.7	235.0	.491E+06	4.88	1.87
50-1	4.76	109.5	123.2	123.5	261.3	251.7	234.2	.486E+06	2.78	1.07

POOR ORIGINAL

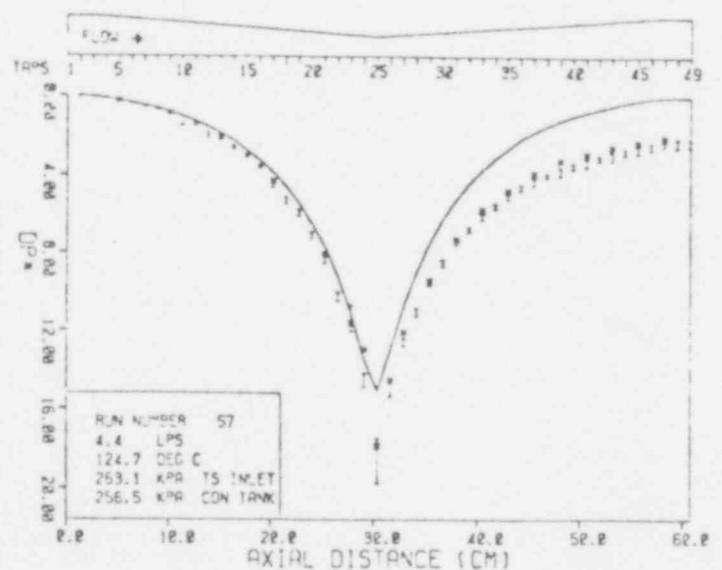
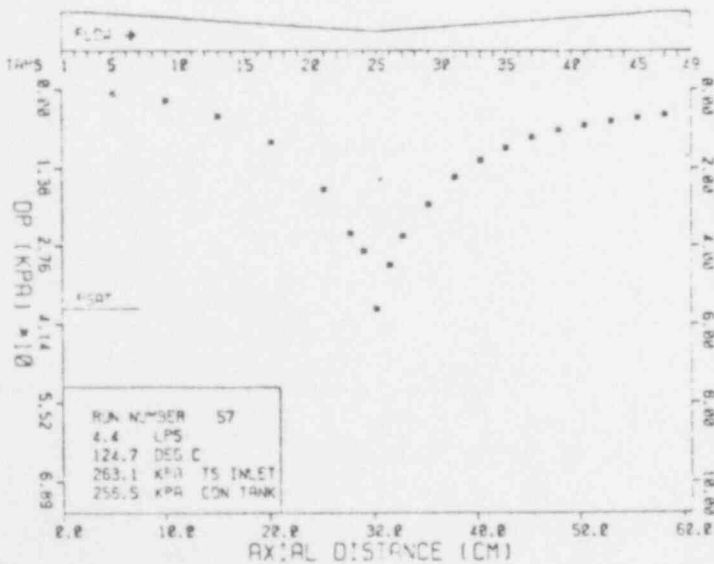


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 57

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM/SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-5	4.32	108.4	123.2	124.8	263.1	256.5	212.9	.442E+06	.52	.24
1-9	4.35	108.3	124.5	124.2	263.1	256.5	214.2	.449E+06	1.88	.87
1-13	4.34	108.3	122.9	123.8	263.1	256.5	213.6	.443E+06	4.58	2.11
1-17	4.33	108.3	124.8	124.1	263.1	256.5	212.4	.446E+06	9.09	4.25
1-21	4.33	108.3	123.0	123.9	263.1	256.5	213.4	.443E+06	17.34	8.03
1-23	4.35	108.2	123.7	123.7	263.1	256.5	214.2	.446E+06	25.21	11.60
1-24	4.34	108.2	124.6	124.0	263.1	256.5	215.7	.452E+06	28.50	12.94
1-25	4.34	108.3	124.6	124.0	263.1	256.5	213.6	.441E+06	34.62	17.35
1-26	4.31	108.1	124.1	123.9	263.1	256.5	212.0	.443E+06	31.98	14.55
1-27	4.32	108.1	124.2	123.9	263.1	256.5	212.6	.445E+06	25.80	12.06
1-29	4.31	108.1	123.6	123.8	263.1	256.5	212.1	.442E+06	21.17	9.46
1-31	4.29	108.1	124.6	123.9	263.1	256.5	211.0	.443E+06	15.32	7.27
1-33	4.32	108.1	124.5	123.7	263.1	256.5	212.8	.446E+06	12.32	5.74
1-35	4.33	108.1	124.6	123.9	263.1	256.5	213.1	.447E+06	10.22	4.76
1-37	4.34	108.1	124.1	123.9	263.1	256.5	211.8	.443E+06	8.26	3.89
1-39	4.32	108.1	124.7	123.9	263.1	256.5	213.0	.447E+06	6.98	3.15
1-41	4.30	108.2	122.7	123.6	263.1	256.5	211.8	.438E+06	6.18	2.90
1-43	4.34	108.1	124.7	123.8	263.1	256.5	213.8	.449E+06	5.48	2.53
1-45	4.29	108.1	124.1	123.7	263.1	256.5	211.4	.442E+06	4.90	2.12
1-47	4.30	108.2	122.9	123.7	263.1	256.5	211.8	.439E+06	4.44	2.10
1-49	4.31	108.2	123.5	123.9	263.1	256.5	212.2	.442E+06	4.17	1.95
50-1	4.36	108.2	124.7	123.9	263.1	256.5	214.5	.450E+06	1.65	.76

POOR ORIGINAL

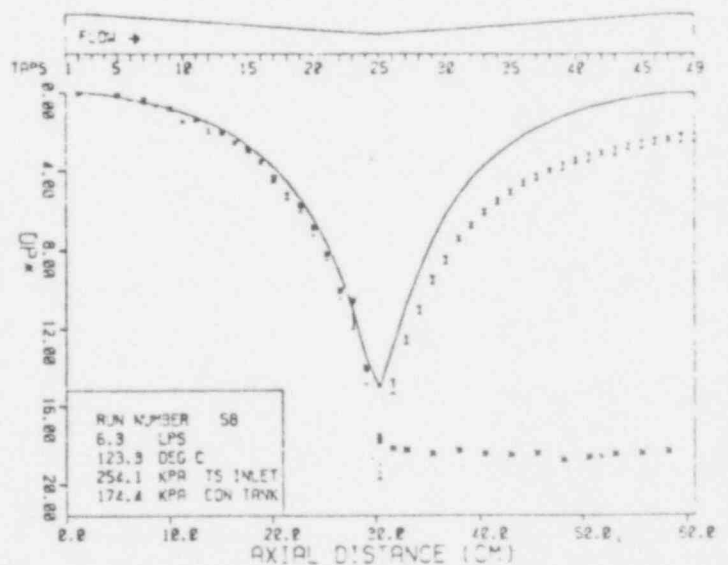
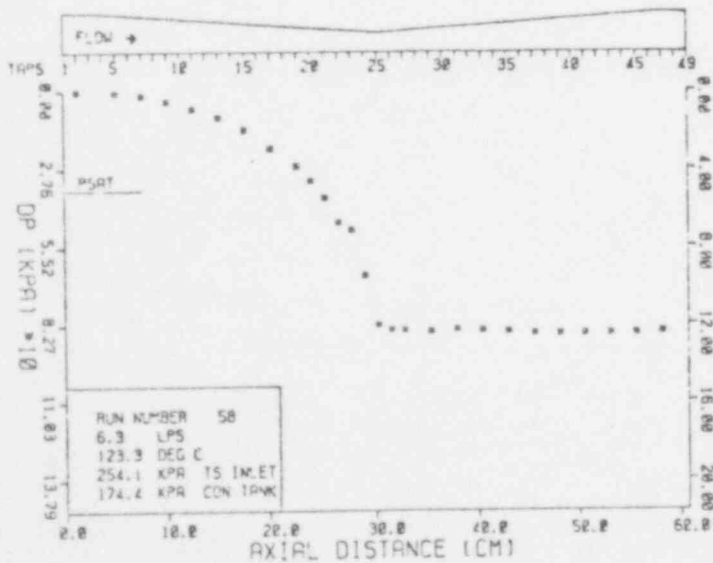


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 58

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	6.38	106.2	123.1	110.2	254.1	174.4	314.2	.652E+06	.15	.03
1-5	6.37	106.2	123.1	110.3	254.1	174.4	313.7	.651E+06	.58	.12
1-7	6.36	106.2	123.1	110.3	254.1	174.4	313.1	.650E+06	1.64	.35
1-9	6.35	106.2	123.2	110.3	254.1	174.4	312.7	.649E+06	3.79	.82
1-11	6.38	106.2	123.1	110.2	254.1	174.4	314.3	.652E+06	6.31	1.35
1-13	6.37	106.2	123.1	110.3	254.1	174.4	313.4	.651E+06	9.46	2.03
1-15	6.37	106.3	123.2	110.2	254.1	174.4	313.8	.651E+06	13.85	2.97
1-17	6.34	106.2	123.2	110.3	254.1	174.4	312.4	.649E+06	20.45	4.42
1-19	6.36	106.2	123.1	110.3	254.1	174.4	313.2	.650E+06	26.60	5.72
1-20	6.36	106.2	123.2	110.3	254.1	174.4	313.8	.650E+06	31.72	6.83
1-21	6.35	106.2	123.1	110.2	254.1	174.4	312.9	.649E+06	37.88	8.16
1-22	6.36	106.2	123.1	110.2	254.1	174.4	313.0	.649E+06	46.55	10.07
1-23	6.34	106.2	123.0	110.1	254.1	174.4	313.9	.651E+06	49.29	10.55
1-24	6.35	106.1	123.0	110.1	254.1	174.4	312.7	.648E+06	65.05	14.03
1-25	6.36	106.1	122.9	110.0	254.1	174.4	313.1	.649E+06	82.70	17.79
1-26	6.36	106.0	122.9	109.9	254.1	174.4	313.3	.649E+06	84.59	18.18
1-27	6.36	106.0	122.9	110.0	254.1	174.4	313.1	.649E+06	84.85	18.25
1-29	6.34	106.0	122.9	110.0	254.1	174.4	312.3	.647E+06	85.32	18.45
1-31	6.34	106.0	123.2	110.1	254.1	174.4	312.3	.648E+06	84.69	18.37
1-33	6.37	106.0	123.1	110.1	254.1	174.4	311.3	.646E+06	84.96	18.49
1-35	6.37	106.1	123.1	110.1	254.1	174.4	311.8	.647E+06	85.33	18.51
1-37	6.37	106.1	123.2	110.2	254.1	174.4	313.5	.651E+06	86.03	18.47
1-39	6.32	106.1	123.2	110.2	254.1	174.4	311.4	.647E+06	86.34	18.79
1-41	6.34	106.1	123.2	110.3	254.1	174.4	312.1	.648E+06	86.12	18.65
1-43	6.36	106.2	123.2	110.3	254.1	174.4	313.1	.650E+06	86.01	18.51
1-45	6.37	106.2	123.2	110.3	254.1	174.4	313.5	.651E+06	86.01	18.46
1-47	6.36	106.2	123.3	110.3	254.1	174.4	313.4	.651E+06	85.49	18.37
1-49	6.33	106.2	123.3	110.3	254.1	174.4	311.8	.648E+06	85.73	18.60
50-1	6.32	106.3	123.3	110.3	254.1	174.4	311.4	.647E+06	5.80	1.26

POOR ORIGINAL



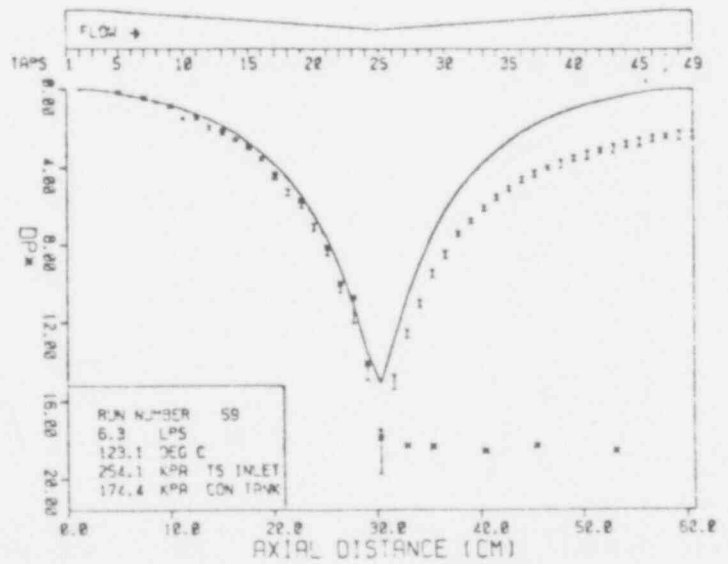
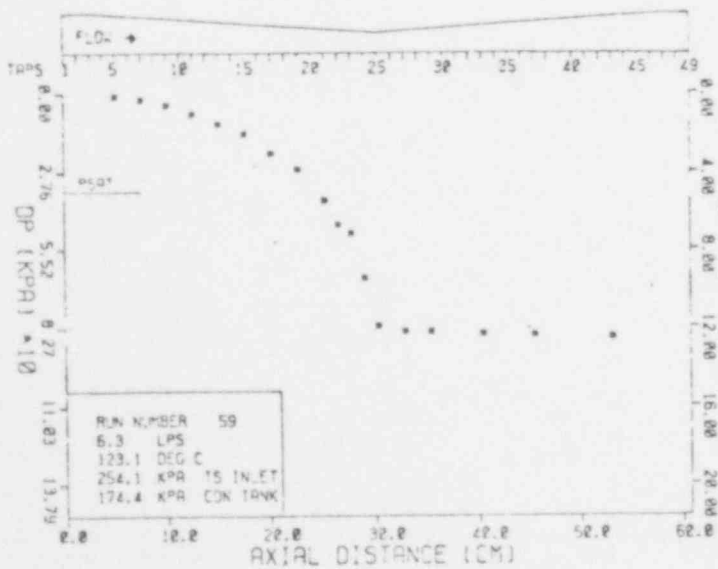


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 59

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE MEASURED DIMENSIONLESS	
		FLOW WATER	TS INLET	COND TANK	TS INLET	COND TANK				
1-5	6.34	106.3	123.3	119.3	254.1	174.4	312.2	.649E+06	.80	.17
1-7	6.35	106.3	123.3	110.3	254.1	174.4	312.5	.649E+06	2.04	.44
1-9	6.34	106.2	123.3	110.3	254.1	174.4	312.2	.649E+06	4.00	.87
1-11	6.35	106.2	123.3	110.3	254.1	174.4	312.6	.650E+06	6.96	1.50
1-13	6.35	106.2	123.3	110.3	254.1	174.4	312.9	.650E+06	10.41	2.24
1-15	6.36	106.2	123.2	110.3	254.1	174.4	313.0	.650E+06	13.76	2.96
1-17	6.33	106.2	123.2	110.2	254.1	174.4	311.7	.647E+06	20.67	4.49
1-19	6.36	106.2	123.2	110.3	254.1	174.4	313.3	.651E+06	26.50	5.69
1-21	6.35	106.2	123.2	110.2	254.1	174.4	312.5	.649E+06	37.62	8.12
1-22	6.33	106.2	123.2	110.2	254.1	174.4	312.8	.650E+06	46.36	9.99
1-23	6.35	106.1	123.2	110.2	254.1	174.4	311.6	.647E+06	49.34	10.72
1-24	6.36	106.1	123.2	110.2	254.1	174.4	313.0	.650E+06	65.19	14.03
1-25	6.33	106.1	123.2	110.2	254.1	174.4	311.5	.647E+06	82.21	17.87
1-27	6.33	106.1	123.1	110.2	254.1	174.4	311.7	.647E+06	84.27	18.29
1-29	6.32	106.1	123.1	110.1	254.1	174.4	311.2	.646E+06	84.19	18.34
1-33	6.31	106.1	123.1	110.2	254.1	174.4	310.9	.645E+06	84.94	18.54
1-37	6.28	106.1	123.1	110.2	254.1	174.4	314.1	.652E+06	85.49	18.27
1-43	6.36	106.1	123.2	110.2	254.1	174.4	313.0	.650E+06	86.19	18.56
1-49	6.34	106.1	123.1	110.2	254.1	174.4	312.2	.648E+06	85.62	18.54
50-1	6.33	106.1	123.1	110.2	254.1	174.4	311.6	.647E+06	5.86	1.27

POOR ORIGINAL



BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 60

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DPO C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-20	6.27	112.9	125.6	112.4	263.7	186.2	309.0	.653E+06	30.64	6.79
1-21	6.26	112.9	125.7	112.4	263.7	186.2	309.1	.654E+06	36.79	8.14
1-22	6.29	113.0	125.8	112.5	263.7	186.2	309.5	.655E+06	45.08	9.95
1-23	6.25	113.0	125.8	112.5	263.7	186.2	307.7	.651E+06	47.22	10.55
1-24	6.27	113.0	125.8	112.5	263.7	186.2	309.0	.654E+06	63.49	14.07
1-25	6.28	113.0	125.8	112.5	263.7	186.2	309.5	.655E+06	80.54	17.79
1-26	6.29	113.0	125.8	112.6	263.7	186.2	309.7	.656E+06	82.26	18.14
1-27	6.27	113.1	125.8	112.6	263.7	186.2	308.9	.654E+06	83.13	18.42
1-29	6.30	113.1	125.8	112.6	263.7	186.2	310.1	.657E+06	83.11	18.27

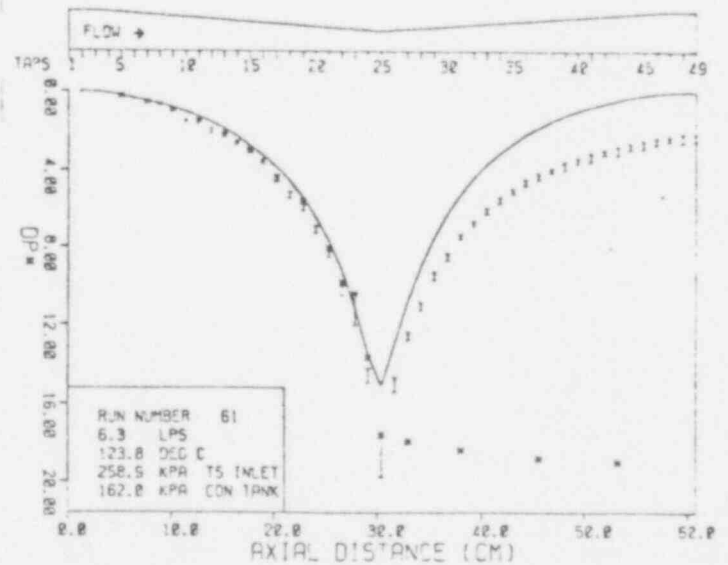
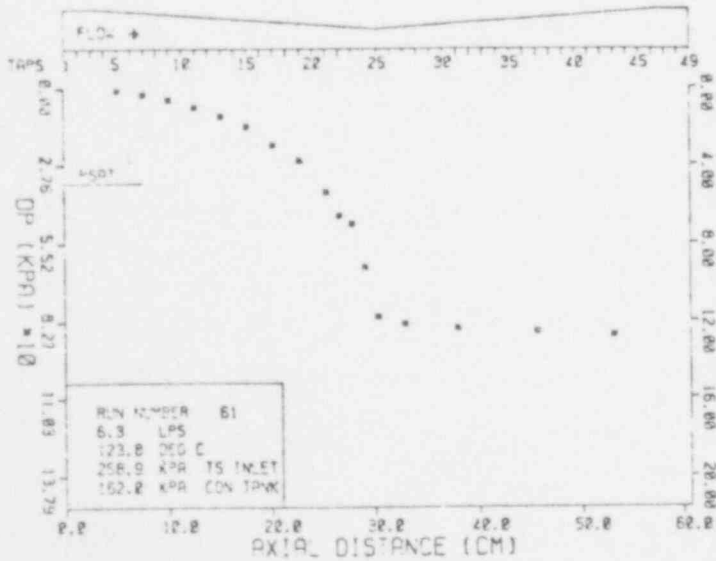
POOR ORIGINAL

BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 61

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-5	6.36	109.2	124.2	108.9	258.9	162.0	313.1	.655E+06	1.09	.23
1-7	6.35	109.2	124.2	108.9	258.9	162.0	312.4	.654E+06	2.47	.54
1-9	6.34	109.3	124.2	108.9	258.9	162.0	312.3	.653E+06	4.22	.93
1-11	6.35	109.3	124.1	108.9	258.9	162.0	312.6	.653E+06	7.05	1.52
1-13	6.33	109.3	124.1	108.9	258.9	162.0	311.5	.651E+06	10.20	2.22
1-15	6.32	109.3	124.1	108.9	258.9	162.0	311.2	.651E+06	13.73	2.99
1-17	6.36	109.3	124.0	108.9	258.9	162.0	313.4	.655E+06	20.54	4.41
1-19	6.36	109.3	124.0	108.9	258.9	162.0	313.0	.654E+06	26.00	5.60
1-21	6.34	109.3	124.0	108.9	258.9	162.0	312.4	.653E+06	37.19	8.04
1-22	6.35	109.3	124.0	108.9	258.9	162.0	312.9	.653E+06	45.52	9.81
1-23	6.36	109.2	124.0	108.8	258.9	162.0	313.2	.654E+06	48.35	10.41
1-24	6.36	109.2	123.9	108.8	258.9	162.0	313.2	.654E+06	63.38	13.64
1-25	6.33	109.2	123.8	108.7	258.9	162.0	311.9	.651E+06	81.01	17.58
1-27	6.37	109.1	123.8	108.7	258.9	162.0	313.8	.655E+06	83.62	17.93
1-31	6.35	109.1	123.8	108.7	258.9	162.0	312.9	.653E+06	85.27	18.39
1-37	6.33	109.0	123.8	108.6	258.9	162.0	311.6	.650E+06	86.39	18.78
1-43	6.34	109.0	123.7	108.5	258.9	162.0	312.3	.651E+06	87.68	18.97
1-49	6.35	108.9	123.7	108.5	258.9	162.0	312.6	.652E+06	87.51	18.90
50-1	6.33	108.9	123.6	108.5	258.9	162.0	311.6	.650E+06	5.91	1.28

POOR ORIGINAL

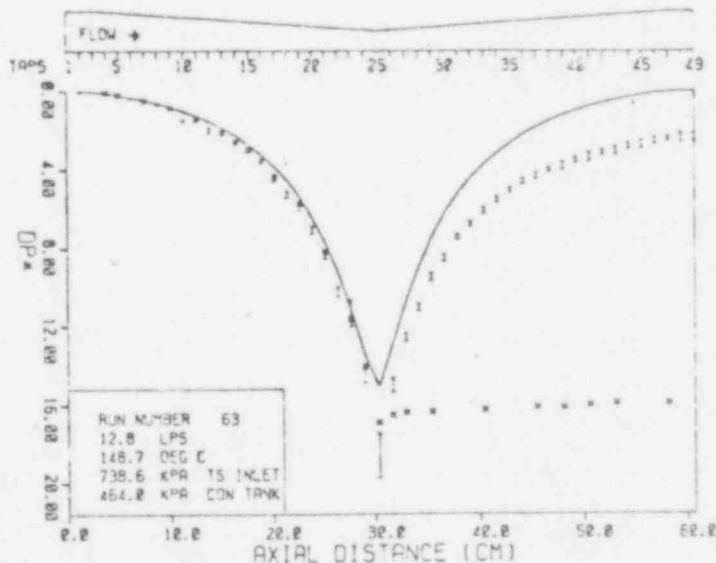
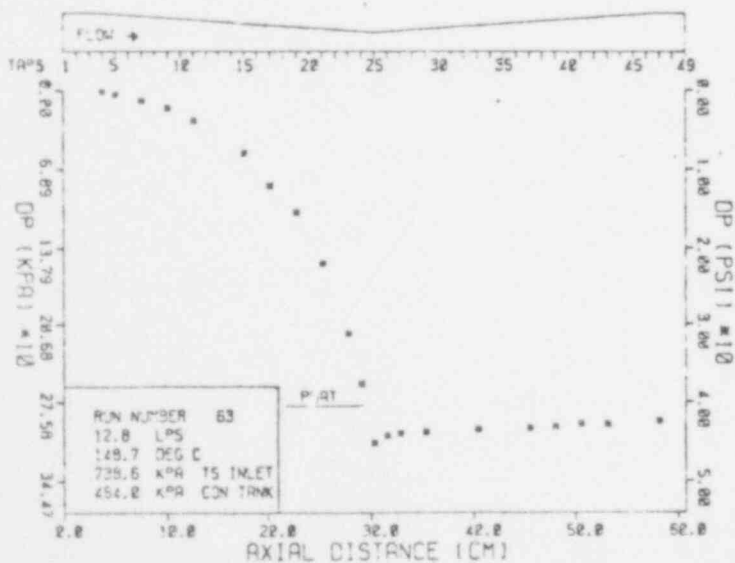


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 63

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-4	12.82	148.4	148.5	148.6	738.6	464.0	631.2	.156E+07	1.53	.08
1-5	12.84	148.5	148.6	148.6	738.6	464.0	632.3	.156E+07	3.64	.20
1-7	12.84	148.5	148.6	148.7	738.6	464.0	632.4	.156E+07	9.29	.50
1-9	12.84	148.5	148.7	148.7	738.6	464.0	632.4	.156E+07	15.89	.86
1-11	12.83	148.6	148.7	148.7	738.6	464.0	632.0	.156E+07	26.82	1.45
1-15	12.83	148.6	148.7	148.7	738.6	464.0	631.6	.156E+07	54.84	2.97
1-17	12.85	148.6	148.7	148.7	738.6	464.0	632.5	.157E+07	82.73	4.47
1-19	12.84	148.6	148.7	148.7	738.6	464.0	632.3	.156E+07	106.31	5.74
1-21	12.85	148.6	148.7	148.7	738.6	464.0	632.9	.157E+07	151.41	8.18
1-23	12.81	148.6	148.7	148.8	738.6	464.0	630.6	.156E+07	214.70	11.66
1-24	12.83	148.6	148.7	148.8	738.6	464.0	632.0	.156E+07	259.66	14.04
1-25	12.81	148.7	148.7	148.8	738.6	464.0	630.7	.156E+07	311.33	16.90
1-26	12.82	148.6	148.7	148.8	738.6	464.0	631.4	.156E+07	304.94	16.52
1-27	12.83	148.6	148.7	148.8	738.6	464.0	631.6	.156E+07	302.88	16.40
1-29	12.82	148.7	148.7	148.8	738.6	464.0	631.1	.156E+07	301.90	16.37
1-31	12.82	148.7	148.7	148.8	738.6	464.0	631.4	.156E+07	300.08	16.26
1-37	12.84	148.6	148.7	148.8	738.6	464.0	632.3	.157E+07	298.16	16.11
1-39	12.81	148.6	148.7	148.7	738.6	464.0	630.7	.156E+07	296.72	16.11
1-41	12.80	148.6	148.7	148.7	738.6	464.0	630.4	.156E+07	294.28	15.99
1-43	12.84	148.6	148.7	148.7	738.6	464.0	632.4	.157E+07	294.64	15.91
1-47	12.79	148.6	148.7	148.7	738.6	464.0	629.9	.156E+07	292.22	15.91
1-49	12.81	148.6	148.7	148.7	738.6	464.0	630.7	.156E+07	291.66	15.84
50-1	12.82	148.6	148.7	148.7	738.6	464.0	631.3	.156E+07	27.45	1.49

POOR ORIGINAL

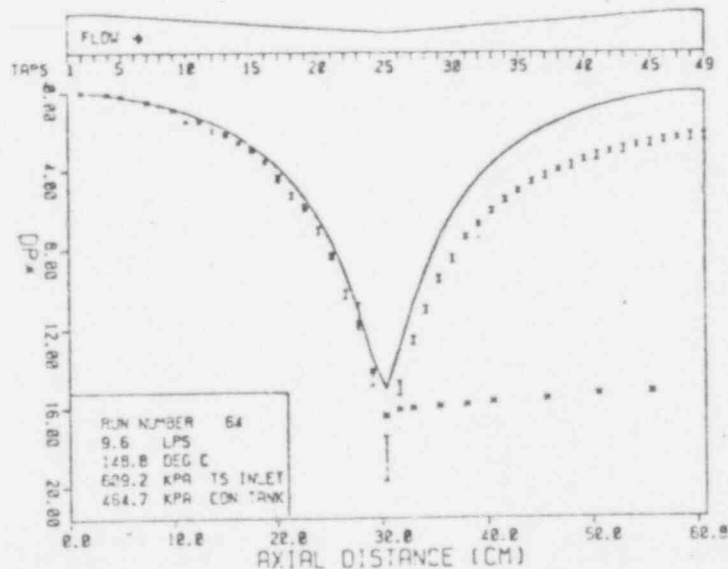
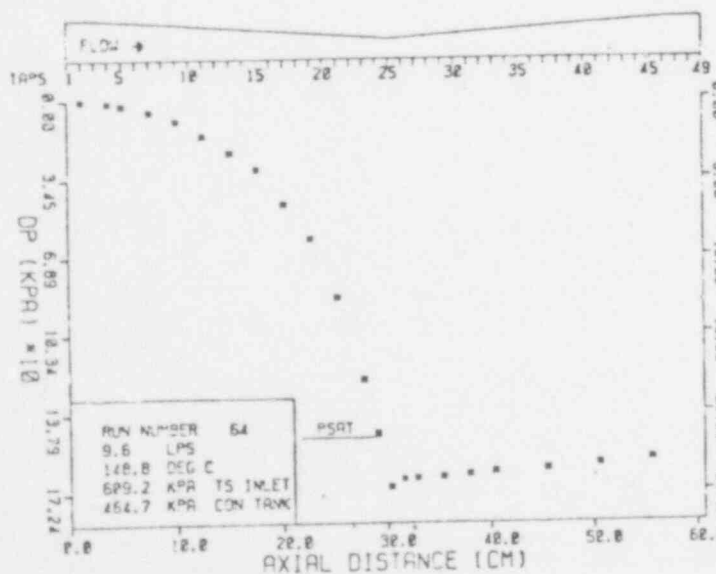


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FAON  
 TEST SECTION # 2

RUN NUMBER 64

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	9.63	138.8	148.8	148.8	609.2	464.7	474.0	.117E+07	.09	.01
1-4	9.62	138.8	148.7	148.7	609.2	464.7	473.8	.117E+07	.79	.08
1-5	9.61	138.0	148.7	148.7	609.2	464.7	473.5	.117E+07	2.10	.20
1-7	9.62	138.0	148.7	148.7	609.2	464.7	473.9	.117E+07	5.04	.49
1-9	9.62	138.0	148.7	148.7	609.2	464.7	473.7	.117E+07	9.12	.88
1-11	9.64	138.0	148.7	148.7	609.2	464.7	475.7	.118E+07	15.47	1.48
1-13	9.64	138.0	148.7	148.7	609.2	464.7	474.6	.118E+07	22.74	2.18
1-15	9.63	138.0	148.7	148.7	609.2	464.7	474.0	.117E+07	30.03	2.89
1-17	9.64	138.1	148.8	148.8	609.2	464.7	474.7	.118E+07	45.33	4.34
1-19	9.64	138.1	148.8	148.8	609.2	464.7	475.8	.118E+07	60.73	5.85
1-21	9.66	138.1	148.8	148.8	609.2	464.7	474.2	.117E+07	86.82	8.34
1-23	9.63	138.1	148.8	148.8	609.2	464.7	476.2	.118E+07	123.11	11.73
1-24	9.62	138.2	148.8	148.8	609.2	464.7	473.6	.117E+07	146.53	14.11
1-25	9.61	138.2	148.8	148.8	609.2	464.7	473.1	.117E+07	170.22	16.43
1-26	9.61	138.2	148.9	148.8	609.2	464.7	473.2	.117E+07	166.90	16.11
1-27	9.62	138.2	148.8	148.8	609.2	464.7	473.5	.117E+07	166.47	16.04
1-29	9.62	138.2	148.8	148.8	609.2	464.7	473.9	.117E+07	166.01	15.97
1-31	9.62	138.3	148.8	148.8	609.2	464.7	473.5	.117E+07	164.87	15.89
1-33	9.64	138.3	148.8	148.8	609.2	464.7	474.7	.118E+07	163.71	15.69
1-35	9.64	138.3	148.8	148.8	609.2	464.7	474.8	.118E+07	162.48	15.57
1-37	9.64	138.3	148.8	148.8	609.2	464.7	475.6	.118E+07	160.46	15.33
1-41	9.66	138.3	148.9	148.9	609.2	464.7	473.5	.117E+07	158.19	15.24
1-45	9.62	138.3	148.8	148.8	609.2	464.7	474.2	.117E+07	154.07	14.80
1-49	9.63	138.3	148.9	148.9	609.2	464.7	474.2	.117E+07	14.82	1.43
50-1	9.62	138.4	148.8	148.8	609.2	464.7	473.8	.117E+07		

POOR ORIGINAL

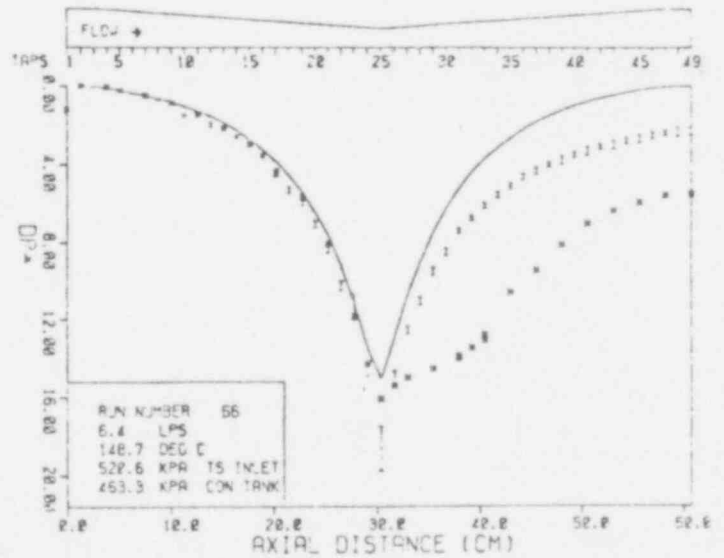
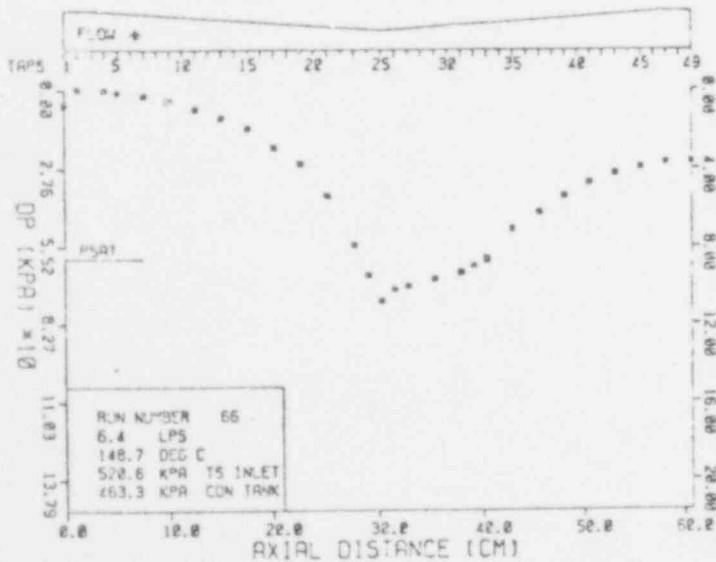


NBL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 66

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	6.39	133.4	148.8	148.7	520.6	463.3	314.9	.780E+06	.02	.00
1-4	6.39	133.4	148.8	148.7	520.6	463.3	314.8	.780E+06	.28	.06
1-4	6.39	133.4	148.8	148.7	520.6	463.3	314.5	.779E+06	.20	.04
1-5	6.37	133.4	148.8	148.8	520.6	463.3	313.8	.777E+06	1.02	.22
1-7	6.43	133.4	148.8	148.8	520.6	463.3	316.8	.785E+06	2.06	.44
1-8	6.38	133.4	148.9	148.8	520.6	463.3	314.3	.779E+06	3.81	.83
1-11	6.39	133.4	148.9	148.8	520.6	463.3	314.5	.779E+06	6.69	1.46
1-13	6.39	133.4	148.8	148.8	520.6	463.3	314.9	.780E+06	9.99	2.18
1-15	6.42	133.4	148.9	148.8	520.6	463.3	315.9	.783E+06	13.57	2.94
1-17	6.39	133.4	148.8	148.8	520.6	463.3	314.7	.780E+06	20.32	4.44
1-19	6.40	133.4	148.8	148.8	520.6	463.3	315.3	.781E+06	25.94	5.64
1-21	6.40	133.4	148.8	148.8	520.6	463.3	314.9	.780E+06	36.95	8.05
1-23	6.41	133.4	148.9	148.8	520.6	463.3	315.6	.782E+06	54.53	11.83
1-24	6.38	133.4	148.8	148.8	520.6	463.3	314.2	.779E+06	65.29	14.29
1-25	6.43	133.4	148.9	148.8	520.6	463.3	316.7	.785E+06	74.63	16.08
1-26	6.38	133.4	148.9	148.8	520.6	463.3	314.3	.779E+06	70.38	15.41
1-27	6.38	133.4	148.9	148.8	520.6	463.3	315.9	.783E+06	69.29	15.00
1-29	6.42	133.4	148.9	148.8	520.6	463.3	315.3	.781E+06	66.85	14.53
1-31	6.40	133.4	148.9	148.8	520.6	463.3	315.4	.782E+06	64.65	14.04
1-31	6.41	133.5	148.8	148.8	520.6	463.3	314.9	.780E+06	60.21	13.12
1-33	6.40	133.4	148.8	148.8	520.6	463.3	315.4	.782E+06	48.83	10.61
1-35	6.41	133.4	148.9	148.8	520.6	463.3	313.3	.776E+06	42.87	9.43
1-37	6.36	133.4	148.8	148.8	520.6	463.3	314.8	.778E+06	37.18	8.13
1-39	6.38	133.5	148.9	148.8	520.6	463.3	315.1	.781E+06	32.37	7.05
1-41	6.40	133.5	148.9	148.8	520.6	463.3	315.4	.782E+06	29.28	6.36
1-43	6.41	133.4	148.8	148.8	520.6	463.3	313.7	.777E+06	26.08	5.92
1-45	6.37	133.4	148.8	148.8	520.6	463.3	313.8	.777E+06	25.44	5.58
1-47	6.37	133.4	148.8	148.8	520.6	463.3	315.2	.781E+06	25.44	5.53
1-49	6.40	133.4	148.8	148.8	520.6	463.3	314.3	.779E+06	5.47	1.20
50-1	6.38	133.4	148.8	148.8	520.6	463.3	316.0	.783E+06	64.20	13.89
1-31	6.42	133.4	148.8	148.7	520.6	463.3	315.2	.781E+06	62.11	13.51
1-37	6.40	133.4	148.7	148.7	520.6	463.3	316.5	.784E+06	59.46	12.83
1-33	6.43	133.4	148.7	148.7	520.6	463.3	313.1	.775E+06	55.25	12.17
1-34	6.36	133.3	148.7	148.7	520.6	463.3	314.6	.779E+06	48.88	10.67

POOR ORIGINAL

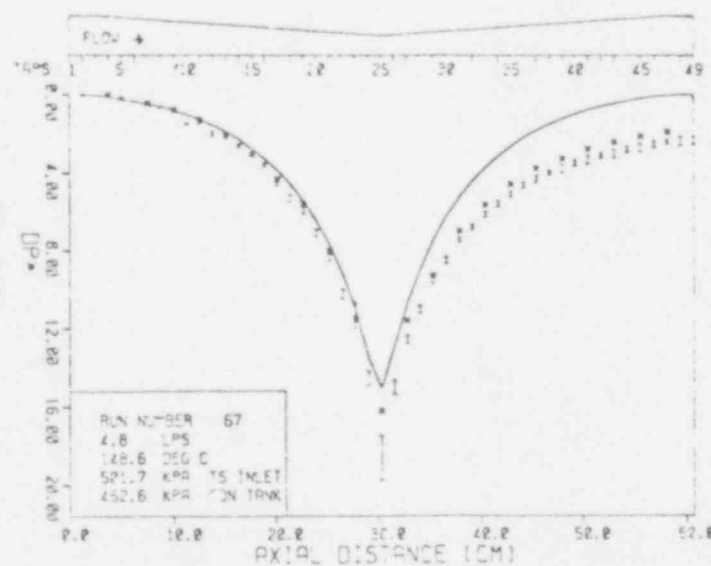
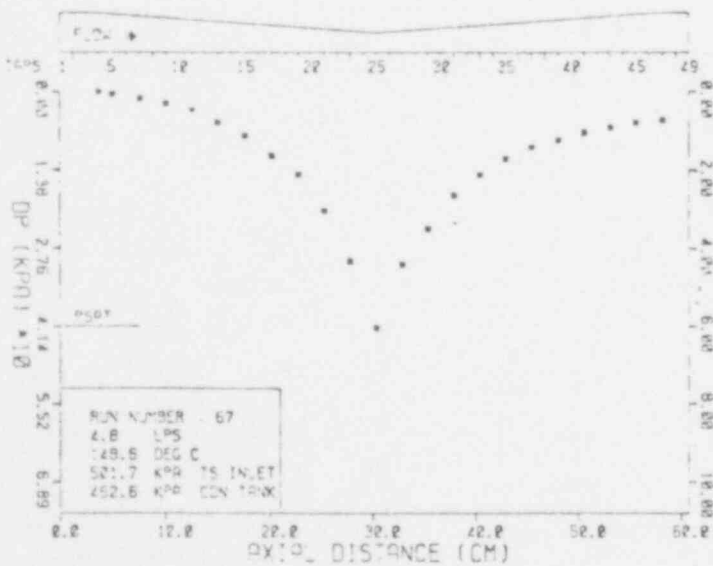


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 67

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-4	4.82	129.3	149.1	149.0	501.7	462.6	237.2	.589E+06	.06	.02
1-5	4.80	129.2	149.1	149.0	501.7	462.6	236.4	.587E+06	.51	.20
1-7	4.80	129.2	149.1	149.0	501.7	462.6	236.4	.587E+06	1.14	.44
1-9	4.81	129.2	149.2	149.0	501.7	462.6	237.0	.588E+06	2.05	.79
1-11	4.82	129.2	149.0	148.9	501.7	462.6	237.3	.589E+06	3.28	1.26
1-13	4.82	129.1	149.2	148.9	501.7	462.6	237.1	.589E+06	5.41	2.08
1-15	4.80	129.1	148.6	148.8	501.7	462.6	236.3	.585E+06	7.80	3.02
1-17	4.83	129.1	149.1	148.9	501.7	462.6	237.9	.590E+06	11.21	4.28
1-19	4.83	129.0	148.7	148.7	501.7	462.6	238.0	.589E+06	14.54	5.54
1-21	4.83	128.9	148.6	148.7	501.7	462.6	237.8	.588E+06	20.89	7.98
1-23	4.80	128.9	148.6	148.7	501.7	462.6	236.3	.585E+06	29.81	11.54
1-25	4.79	128.8	148.7	148.6	501.7	462.6	235.8	.584E+06	41.24	16.19
1-27	4.83	128.8	148.7	148.6	501.7	462.6	238.0	.589E+06	50.42	18.60
1-29	4.81	128.7	148.5	148.5	501.7	462.6	236.7	.585E+06	74.11	28.30
1-31	4.81	128.7	148.6	148.6	501.7	462.6	237.1	.586E+06	88.18	33.99
1-33	4.81	128.7	148.7	148.5	501.7	462.6	237.0	.587E+06	14.63	5.63
1-35	4.80	128.7	148.6	148.5	501.7	462.6	236.3	.584E+06	11.80	4.57
1-37	4.80	128.7	148.6	148.5	501.7	462.6	236.3	.585E+06	9.71	3.76
1-39	4.80	128.7	148.6	148.5	501.7	462.6	236.3	.585E+06	8.50	3.29
1-41	4.81	128.6	148.7	148.5	501.7	462.6	236.8	.586E+06	7.20	2.77
1-43	4.80	128.6	148.7	148.5	501.7	462.6	236.3	.585E+06	6.28	2.43
1-45	4.81	128.7	148.6	148.5	501.7	462.6	236.7	.586E+06	5.48	2.11
1-47	4.83	128.7	148.6	148.6	501.7	462.6	237.6	.588E+06	4.98	1.91
1-49	4.80	128.7	148.7	148.6	501.7	462.6	236.3	.585E+06	4.66	1.80
50:1	4.81	128.7	148.6	148.6	501.7	462.6	237.1	.587E+06	2.26	.87

POOR ORIGINAL

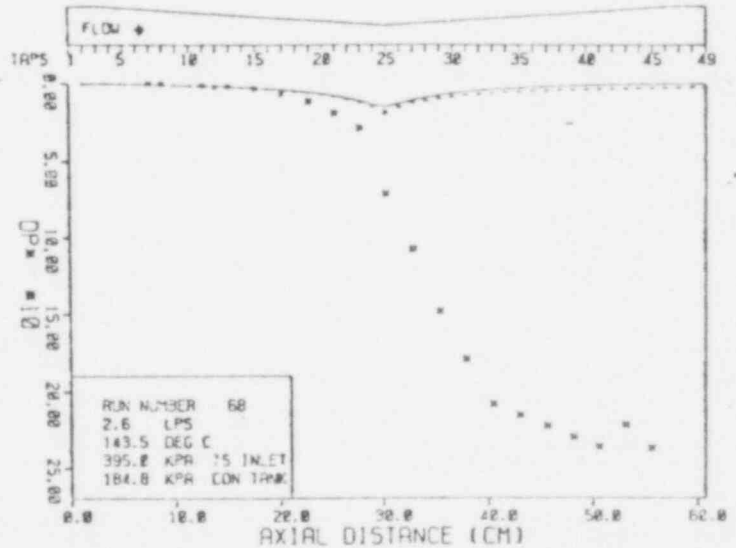
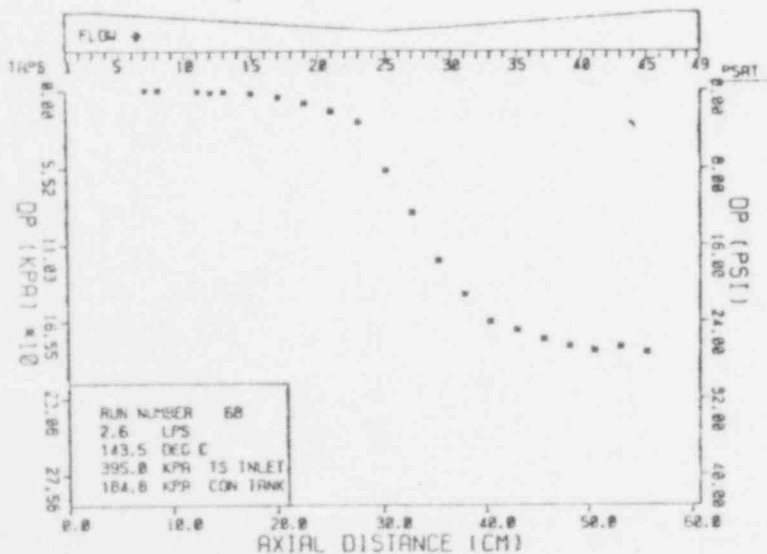


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 68

TAB #	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-7	2.80	116.7	144.1	120.3	395.0	184.8	137.7	.331E+06	.00	.00
1-8	2.67	116.9	144.1	119.0	395.0	184.8	131.2	.316E+06	.00	.00
1-11	2.61	117.0	144.3	118.1	395.0	184.8	128.7	.310E+06	.71	.92
1-13	2.59	116.1	144.3	118.0	395.0	184.8	132.3	.319E+06	1.49	1.83
1-12	2.64	115.4	143.9	118.0	395.0	184.8	130.2	.313E+06	1.67	2.12
1-15	2.66	115.2	143.9	118.9	395.0	184.8	131.2	.315E+06	2.54	3.17
1-17	2.66	115.6	143.8	117.5	395.0	184.8	131.0	.314E+06	4.91	6.16
1-19	2.68	115.1	143.8	117.5	395.0	184.8	131.7	.316E+06	9.06	11.23
1-21	2.64	114.6	143.6	117.2	395.0	184.8	130.1	.312E+06	14.87	18.88
1-23	2.65	114.4	143.6	117.2	395.0	184.8	130.7	.313E+06	22.72	28.60
1-25	2.66	114.3	143.3	117.5	395.0	184.8	130.9	.313E+06	56.71	71.13
1-27	2.68	114.2	143.4	117.4	395.0	184.8	131.9	.316E+06	86.88	107.42
1-29	2.70	114.3	143.5	117.6	395.0	184.8	132.8	.318E+06	121.39	148.03
1-31	2.69	114.5	143.5	118.1	395.0	184.8	132.2	.317E+06	145.63	179.03
1-33	2.66	114.6	143.5	117.7	395.0	184.8	130.9	.313E+06	165.67	207.94
1-35	2.66	114.6	143.6	117.7	395.0	184.8	130.9	.314E+06	171.64	215.37
1-37	2.67	114.6	143.6	118.0	395.0	184.8	131.3	.315E+06	178.11	222.16
1-39	2.66	114.6	143.4	117.8	395.0	184.8	130.9	.313E+06	183.12	229.86
1-41	2.65	114.5	143.6	117.7	395.0	184.8	130.3	.312E+06	186.17	235.43
1-43	2.71	114.5	143.5	117.7	395.0	184.8	131.4	.315E+06	183.42	231.71
1-45	2.65	114.4	143.4	117.8	395.0	184.8	131.3	.312E+06	187.30	237.99
1-47	2.64	114.4	143.4	117.8	395.0	184.8	129.9	.311E+06	186.14	237.18
1-49	2.65	114.4	143.5	118.0	395.0	184.8	130.3	.312E+06	187.84	237.74

POOR ORIGINAL



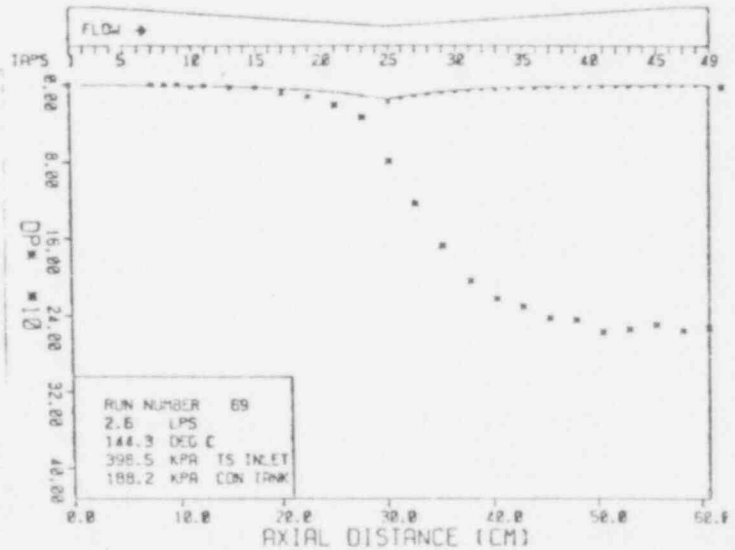
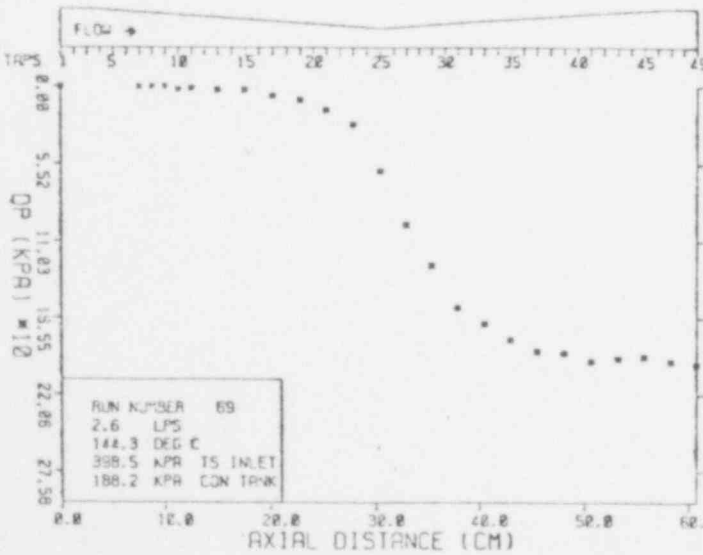


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 69

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SUC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-7	2.62	115.3	144.6	118.6	398.5	188.2	129.0	.311E+06	.00	.00
1-8	2.63	115.2	144.4	118.8	398.5	188.2	129.3	.311E+06	.00	.00
1-9	2.64	115.3	144.3	118.7	398.5	188.2	130.0	.313E+06	.00	.00
1-10	2.61	115.3	144.3	118.6	398.5	188.2	128.6	.310E+06	1.86	2.41
1-11	2.61	115.2	144.3	118.8	398.5	188.2	128.4	.309E+06	1.03	1.34
1-13	2.62	115.2	144.5	118.6	398.5	188.2	128.8	.310E+06	2.08	2.69
1-15	2.63	115.3	144.4	118.7	398.5	188.2	129.4	.312E+06	2.36	3.04
1-17	2.63	115.1	144.4	118.6	398.5	188.2	129.5	.312E+06	6.52	8.37
1-19	2.65	115.1	144.3	118.4	398.5	188.2	130.5	.314E+06	9.68	12.23
1-21	2.62	115.0	144.4	118.5	398.5	188.2	128.9	.311E+06	16.44	21.28
1-23	2.65	115.1	144.4	118.6	398.5	188.2	130.6	.315E+06	27.00	34.04
1-25	2.60	115.0	144.3	118.5	398.5	188.2	128.3	.309E+06	60.12	78.64
1-27	2.66	115.1	144.2	118.5	398.5	188.2	130.8	.315E+06	98.34	123.61
1-29	2.60	115.1	144.5	118.5	398.5	188.2	128.0	.308E+06	127.57	167.61
1-31	2.62	115.1	144.4	118.5	398.5	188.2	129.1	.311E+06	157.94	203.99
1-33	2.60	114.9	144.5	118.5	398.5	188.2	128.1	.309E+06	169.57	222.40
1-35	2.64	115.0	144.4	118.6	398.5	188.2	129.9	.313E+06	181.01	230.69
1-37	2.63	115.0	144.4	118.5	398.5	188.2	129.6	.312E+06	189.20	242.50
1-39	2.63	115.0	144.3	118.4	398.5	188.2	129.6	.312E+06	190.59	244.01
1-41	2.61	114.9	144.3	118.6	398.5	188.2	128.4	.309E+06	196.73	244.87
1-43	2.61	115.1	144.4	118.5	398.5	188.2	128.4	.309E+06	194.74	249.18
1-45	2.62	115.1	144.3	118.6	398.5	188.2	129.2	.311E+06	193.36	249.14
1-47	2.61	115.0	144.2	118.5	398.5	188.2	128.7	.310E+06	196.63	255.50
1-49	2.65	115.0	144.6	118.5	398.5	188.2	130.3	.314E+06	199.25	252.53
50-1	2.64	115.0	144.4	118.6	398.5	188.2	129.8	.313E+06	.00	.00
1-50	2.60	115.0	144.6	118.5	398.5	188.2	127.9	.308E+06	1.76	2.32
1-7	2.63	115.0	144.3	118.6	398.5	188.2	129.3	.311E+06	.00	.00
1-7	2.63	115.1	144.4	118.4	398.5	188.2	129.7	.313E+06	.00	.00
1-9	2.60	114.9	144.3	118.4	398.5	188.2	128.2	.309E+06	.00	.00
1-10	2.62	114.9	144.3	118.2	398.5	188.2	129.1	.311E+06	1.80	2.33

POOR ORIGINAL



APPENDIX C

PRESSURE AND VOID FRACTION DISTRIBUTIONS  
UNDER FLASHING CONDITIONS

## FLASHING EXPERIMENTS

RUN	$P_{in}$ (kPa)	$T_{in}$ ( $^{\circ}$ C)	$G$ (Mg/m <sup>2</sup> s)	$P_{ct}$ (kPa)	$T_{ct}$ ( $^{\circ}$ C)
72	----	----	----	----	-----
73	275.	99.4	4.90	56.	87.9
731*	281.	99.4	4.88	52.	88.0
732*	285.	99.4	4.93	52.	87.9
733*	288.	99.4	4.91	53.	88.2
734*	287.	99.4	4.91	54.	88.0
735*	287.	99.4	4.91	55.	88.1
736*	287.	99.4	4.90	54.	88.0
737*	287.	99.4	4.91	54.	87.9
74	285.	99.3	4.90	56.	87.9
75	395.	99.3	6.04	57.	88.5
761	396.	99.3	6.04	60.	88.7
762	393.	99.3	6.05	62.	88.0
763	392.	99.3	6.06	65.	88.0
77	157.	99.3	3.06	65.	88.7
771	157.	99.4	3.03	69.	88.3
78	138.	99.3	2.61	71.	88.0
782	138.	99.3	2.61	71.	88.1
79	124.	99.4	2.27	72.	88.2
791	126.	99.4	2.26	73.	88.1
792	126.	99.4	2.26	83.	88.1
80	585.	148.3	4.36	436.	143.5
803	579.	148.3	4.32	432.	143.5
81	493.	148.3	2.91	432.	144.0
811	493.	148.3	2.91	432.	144.7
814	492.	148.3	2.91	428.	144.1
82	376.	142.3	2.36	174.	111.6
823	377.	142.4	2.32	176.	110.9
83	352.	140.0	2.30	150.	107.9
833	348.	139.5	2.29	145.	107.1

\*Runs 731 through 737 are subsets of Run 73 as are other runs in the hundreds subsets of their decade base.

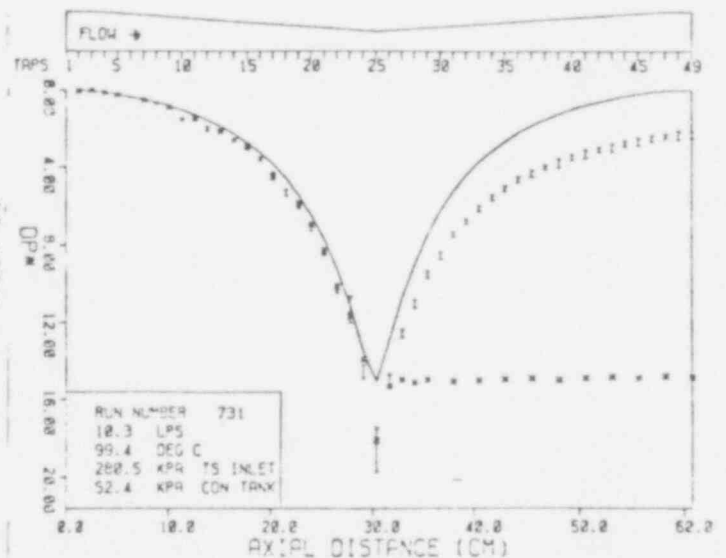
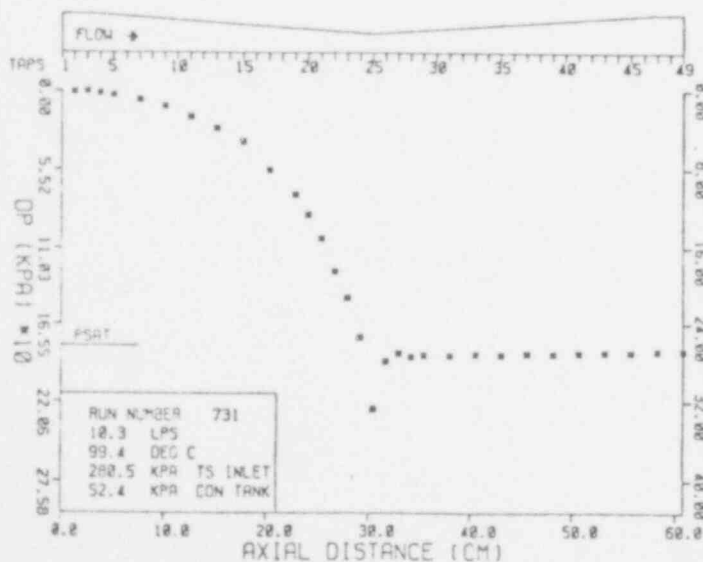


BNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER 731

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	10.33	96.2	99.4	88.1	280.7	52.3	508.5	.862E+06	.43	.03
1-3	10.33	96.2	99.4	87.7	279.7	52.6	508.7	.863E+06	.00	.00
1-4	10.35	96.2	99.4	87.6	280.5	52.5	509.8	.865E+06	1.29	.10
1-5	10.33	96.3	99.4	89.4	279.0	51.5	508.8	.863E+06	2.81	.22
1-7	10.33	96.3	99.4	88.3	281.3	52.1	508.9	.863E+06	6.08	.49
1-9	10.34	96.3	99.4	88.2	281.1	52.2	509.1	.863E+06	10.66	.85
1-11	10.32	96.2	99.4	88.0	280.8	52.4	508.3	.862E+06	18.16	1.45
1-13	10.30	96.3	99.4	87.8	280.8	52.4	507.2	.860E+06	26.43	2.13
1-15	10.33	96.3	99.4	88.0	280.2	52.2	508.8	.863E+06	35.76	2.86
1-17	10.32	96.3	99.4	87.8	281.0	52.3	508.3	.862E+06	55.82	4.47
1-19	10.33	96.3	99.4	87.7	279.8	52.4	508.5	.862E+06	72.49	5.80
1-20	10.36	96.3	99.4	87.8	281.3	52.4	509.9	.865E+06	86.61	6.89
1-21	10.32	96.3	99.4	87.7	280.7	52.5	508.3	.862E+06	103.05	8.25
1-22	10.31	96.3	99.4	87.9	280.7	52.6	507.9	.861E+06	126.62	10.16
1-23	10.33	96.3	99.4	87.9	281.1	52.5	508.8	.863E+06	145.82	11.65
1-24	10.35	96.3	99.4	87.8	281.4	52.6	509.6	.864E+06	174.49	13.90
1-25	10.30	96.3	99.4	87.8	279.2	52.6	507.6	.864E+06	225.19	18.13
1-26	10.35	96.3	99.4	88.0	278.9	52.7	509.6	.864E+06	192.09	15.31
1-27	10.31	96.3	99.4	87.8	280.1	52.7	507.6	.861E+06	186.18	14.55
1-28	10.32	96.3	99.4	87.8	280.3	52.8	508.1	.862E+06	188.68	15.12
1-29	10.33	96.3	99.4	87.6	279.5	52.7	508.9	.863E+06	187.47	14.98
1-31	10.32	96.3	99.4	88.7	279.3	52.2	508.0	.861E+06	187.84	14.96
1-33	10.32	96.3	99.4	88.1	280.4	52.3	508.1	.862E+06	187.37	15.02
1-35	10.35	96.3	99.4	87.9	281.2	52.4	509.8	.864E+06	187.52	14.93
1-37	10.33	96.3	99.4	87.9	280.4	52.6	508.9	.863E+06	186.51	14.91
1-39	10.32	96.3	99.4	87.7	280.8	52.7	508.2	.862E+06	186.82	14.97
1-41	10.33	96.3	99.4	87.8	281.4	52.6	508.6	.863E+06	186.29	14.90
1-43	10.34	96.3	99.4	89.5	280.1	51.9	509.1	.863E+06	185.85	14.84
1-45	10.32	96.3	99.4	88.5	279.8	52.3	508.3	.862E+06	185.92	14.89
1-47	10.34	96.3	99.4	88.2	280.2	52.4	509.0	.863E+06	185.18	14.79
1-49	10.30	96.3	99.4	88.2	280.9	52.6	507.3	.860E+06	184.80	14.86
50-1	10.32	96.3	99.4	87.9	281.5	52.7	508.2	.862E+06	17.71	1.42

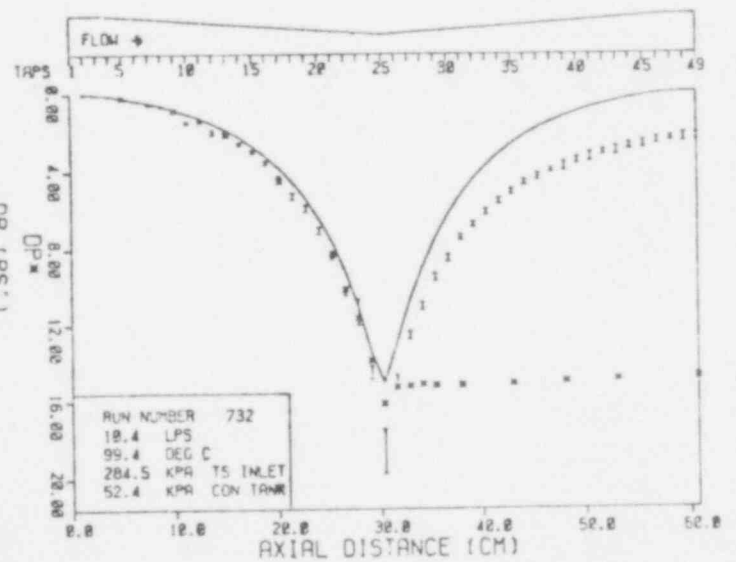
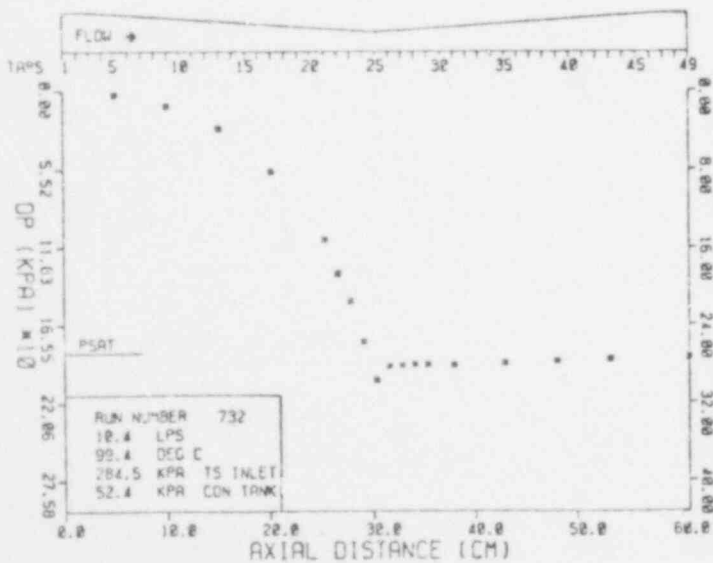
POOR ORIGINAL



BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM/SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
RUN NUMBER 732										
1-5	10.44	96.3	99.4	88.1	284.8	52.5	514.2	.872E+06	2.65	.21
1-9	10.41	96.4	99.4	88.1	284.7	52.1	512.4	.869E+06	10.79	.85
1-13	10.42	96.3	99.3	87.7	283.7	52.2	513.3	.870E+06	26.88	2.11
1-17	10.42	96.3	99.3	87.8	283.8	52.3	513.1	.870E+06	56.94	4.48
1-21	10.43	96.3	99.3	87.6	284.3	52.2	513.6	.870E+06	104.94	8.23
1-22	10.40	96.3	99.3	87.9	283.5	52.4	512.3	.868E+06	128.94	10.17
1-23	10.42	96.3	99.3	87.6	285.2	52.4	513.2	.870E+06	148.43	11.66
1-24	10.45	96.3	99.3	87.7	284.4	52.6	514.4	.872E+06	177.34	13.57
1-25	10.40	96.3	99.4	88.2	283.6	52.3	512.0	.868E+06	204.39	16.14
1-26	10.43	96.3	99.4	87.7	283.6	52.4	511.4	.871E+06	194.83	15.30
1-27	10.43	96.3	99.4	87.9	284.8	52.6	511.4	.870E+06	194.14	15.24
1-28	10.44	96.4	99.4	87.8	285.3	52.6	514.0	.872E+06	193.27	15.14
1-29	10.43	96.3	99.4	88.0	284.7	52.2	513.5	.871E+06	193.66	15.20
1-31	10.43	96.4	99.4	88.2	285.0	52.3	513.8	.871E+06	193.77	15.19
1-35	10.43	96.4	99.4	88.1	284.3	52.5	513.4	.870E+06	192.67	15.13
1-39	10.44	96.4	99.4	87.8	285.9	52.6	513.9	.871E+06	191.51	15.01
1-43	10.42	96.4	99.4	87.5	284.4	52.6	513.3	.870E+06	189.91	14.92
1-49	10.43	96.3	99.4	88.3	285.0	52.2	513.5	.871E+06	188.91	14.83
50-1	10.44	96.3	99.4	88.5	285.0	52.4	514.2	.872E+06	17.83	1.40

POOR ORIGINAL



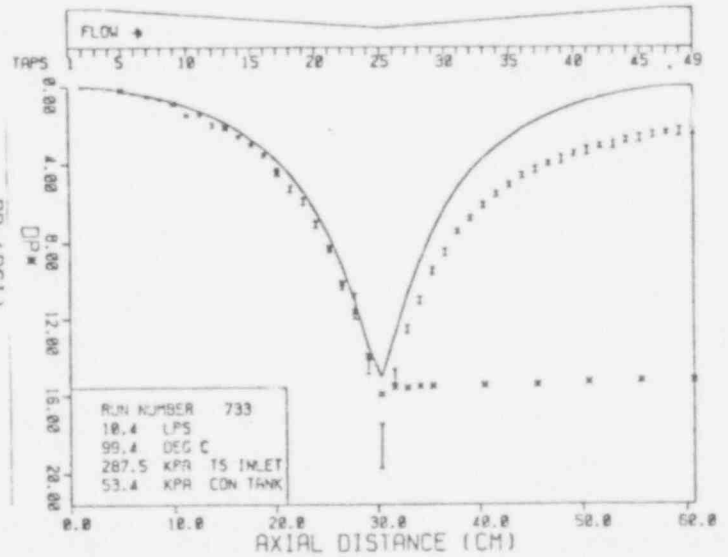
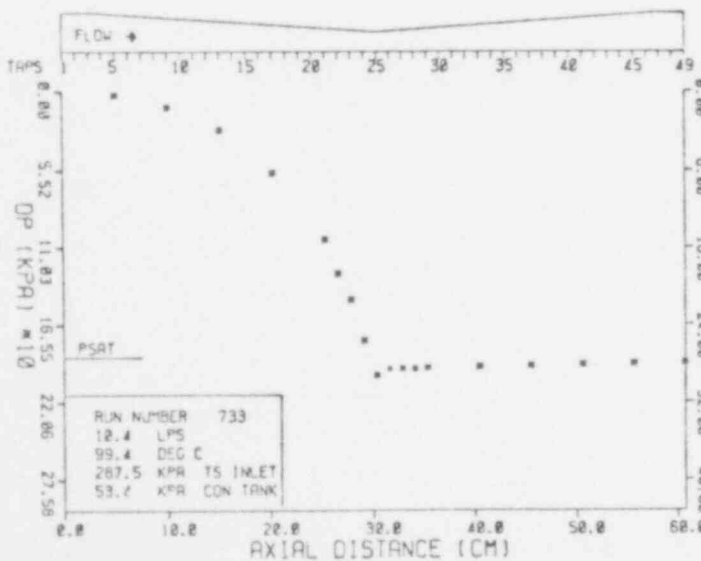
575 192

BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 733

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-5	10.37	96.4	99.4	87.9	288.9	53.3	510.9	.866E+06	2.62	.21
1-9	10.37	96.3	99.4	87.7	287.7	53.4	510.7	.866E+06	11.03	.89
1-13	10.38	96.4	99.4	88.0	288.2	53.5	511.1	.867E+06	26.71	2.12
1-17	10.39	96.4	99.4	88.4	287.5	53.1	511.6	.867E+06	56.60	4.48
1-21	10.37	96.4	99.4	88.1	287.4	53.3	510.5	.866E+06	104.29	8.28
1-22	10.40	96.4	99.4	87.7	287.8	53.5	512.2	.869E+06	128.41	10.13
1-23	10.40	96.4	99.4	88.3	288.1	53.1	512.1	.868E+06	147.48	11.64
1-24	10.39	96.4	99.4	88.2	287.4	53.3	511.6	.868E+06	176.64	13.97
1-25	10.38	96.4	99.4	88.3	286.2	53.4	511.4	.868E+06	201.29	15.93
1-26	10.39	96.4	99.4	88.0	287.5	53.5	511.6	.868E+06	197.03	15.58
1-27	10.36	96.4	99.4	88.4	288.1	53.5	510.3	.865E+06	196.66	15.11
1-28	10.40	96.4	99.4	87.9	287.2	53.6	512.2	.869E+06	197.02	15.54
1-29	10.37	96.4	99.4	88.0	287.4	53.7	510.7	.866E+06	195.72	15.53
1-33	10.38	96.4	99.4	87.8	287.3	53.6	511.1	.866E+06	195.47	15.49
1-37	10.37	96.4	99.4	87.7	287.4	53.7	510.6	.866E+06	194.60	15.45
1-41	10.40	96.4	99.4	89.2	287.0	53.1	512.0	.868E+06	193.92	15.31
1-45	10.40	96.4	99.4	88.7	288.1	53.4	512.2	.868E+06	193.10	15.23
1-49	10.37	96.4	99.4	88.6	286.9	53.6	510.9	.866E+06	192.47	15.26
50-1	10.38	96.4	99.4	88.3	286.8	53.7	511.4	.867E+06	17.86	1.44

POOR ORIGINAL

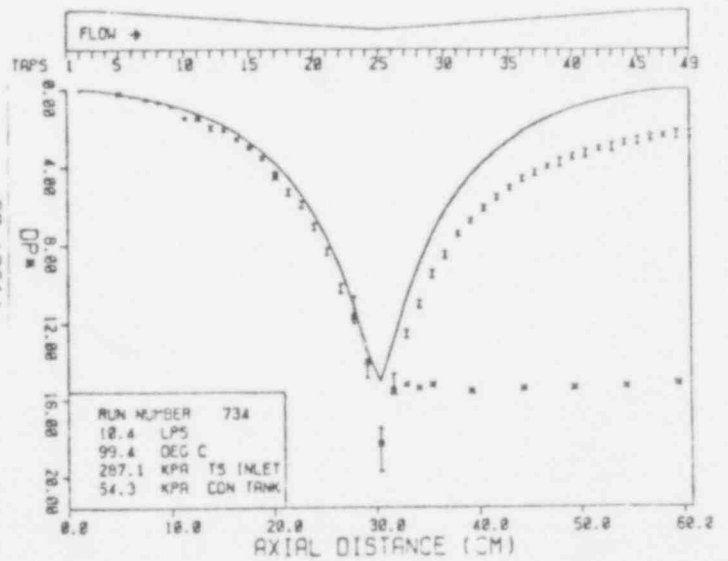
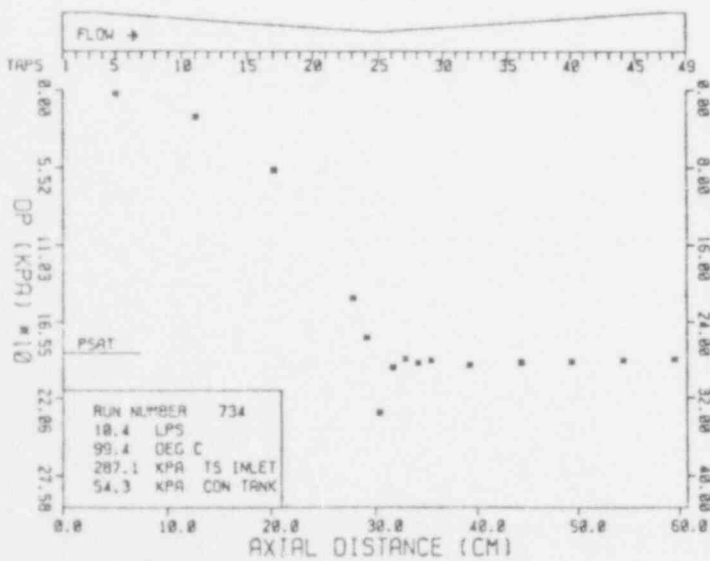


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 734

TAPS	LOOP FLOW LTM/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-5	10.36	96.3	99.4	88.0	287.5	54.1	510.0	.865E+06	2.56	.20
1-11	10.39	96.3	99.4	88.0	287.0	54.1	511.4	.867E+06	18.67	1.48
1-17	10.37	96.4	99.4	87.9	287.3	54.2	510.9	.866E+06	56.49	4.48
1-23	10.38	96.3	99.4	88.1	287.2	54.3	511.2	.867E+06	147.77	11.70
1-24	10.38	96.3	99.4	88.0	287.8	54.3	511.3	.867E+06	176.53	13.97
1-25	10.38	96.3	99.4	88.0	288.2	54.3	511.0	.866E+06	230.54	18.31
1-26	10.41	96.3	99.4	88.0	286.9	54.4	512.7	.869E+06	198.41	15.62
1-27	10.39	96.3	99.4	87.5	287.8	54.5	511.7	.868E+06	192.33	15.20
1-28	10.40	96.3	99.4	88.6	286.7	54.0	512.0	.868E+06	194.86	15.39
1-29	10.42	96.3	99.4	88.3	285.0	54.2	513.0	.870E+06	193.49	15.22
1-32	10.39	96.3	99.4	88.0	287.7	54.3	511.9	.868E+06	196.70	15.54
1-36	10.39	96.3	99.4	88.2	287.7	54.4	511.8	.868E+06	194.96	15.40
1-40	10.39	96.3	99.4	88.1	286.9	54.4	511.5	.867E+06	194.41	15.38
1-44	10.38	96.3	99.4	87.9	287.4	54.5	511.3	.867E+06	193.52	15.32
1-48	10.41	96.3	99.4	88.0	286.9	54.6	512.4	.869E+06	192.69	15.19
50-1	10.40	96.3	99.4	87.9	286.3	54.5	512.0	.868E+06	17.96	1.42

POOR ORIGINAL



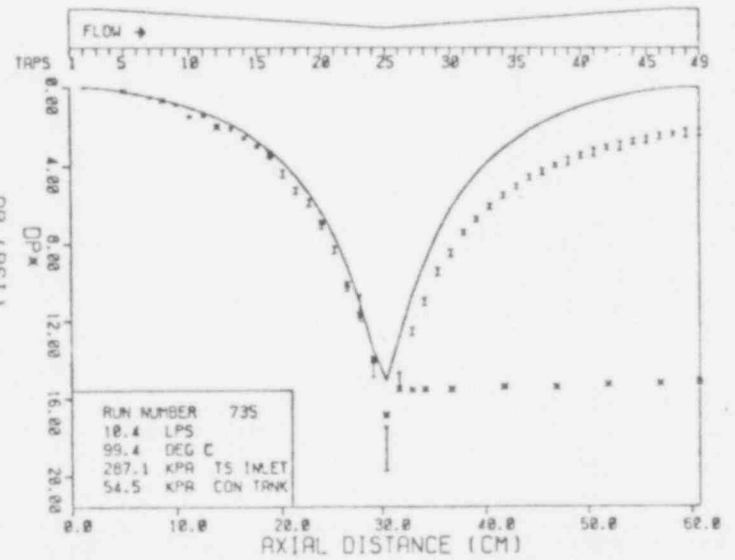
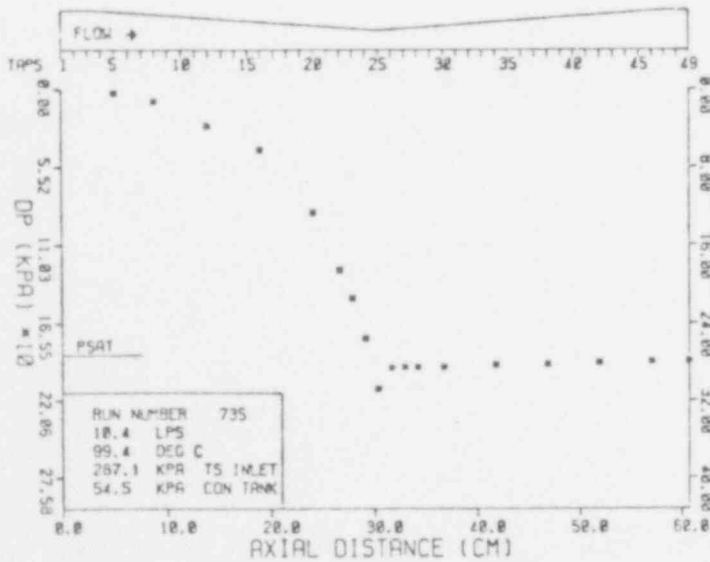


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 735

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-5	10.36	96.3	99.4	88.1	286.9	54.2	510.3	.865E+06	2.49	.20
1-8	10.37	96.3	99.3	88.3	286.0	54.4	510.5	.865E+06	8.30	.66
1-12	10.38	96.3	99.4	88.1	287.5	54.4	511.0	.866E+06	25.53	2.02
1-16	10.38	96.3	99.4	88.3	287.0	54.5	511.0	.866E+06	42.67	3.38
1-20	10.40	96.3	99.3	88.0	287.1	54.5	511.9	.868E+06	87.39	6.90
1-22	10.38	96.3	99.4	87.7	286.8	54.6	510.9	.866E+06	128.08	10.15
1-23	10.38	96.3	99.4	88.0	287.5	54.5	511.1	.866E+06	147.78	11.71
1-24	10.37	96.3	99.4	88.2	287.1	54.6	510.5	.866E+06	175.94	13.97
1-25	10.35	96.3	99.4	88.2	286.6	54.7	509.9	.864E+06	212.01	16.88
1-26	10.40	96.3	99.4	88.2	286.8	54.4	512.2	.868E+06	197.00	15.54
1-27	10.38	96.3	99.4	88.0	286.0	54.6	511.2	.867E+06	196.40	15.56
1-28	10.39	96.3	99.4	88.1	287.7	54.6	511.7	.868E+06	196.56	15.54
1-30	10.39	96.3	99.4	88.1	287.8	54.7	511.7	.868E+06	196.69	15.55
1-34	10.40	96.3	99.4	88.3	288.3	54.8	512.0	.868E+06	194.99	15.40
1-38	10.38	96.3	99.4	88.3	286.4	54.3	510.9	.866E+06	194.46	15.42
1-42	10.38	96.3	99.4	88.1	287.2	54.5	511.2	.867E+06	193.29	15.31
1-46	10.38	96.3	99.4	88.1	286.3	54.6	511.3	.867E+06	192.64	15.25
1-49	10.41	96.3	99.4	87.9	288.3	54.6	512.5	.869E+06	192.21	15.14
50-1	10.39	96.3	99.4	87.6	287.0	54.6	511.4	.867E+06	17.92	1.42

POOR ORIGINAL

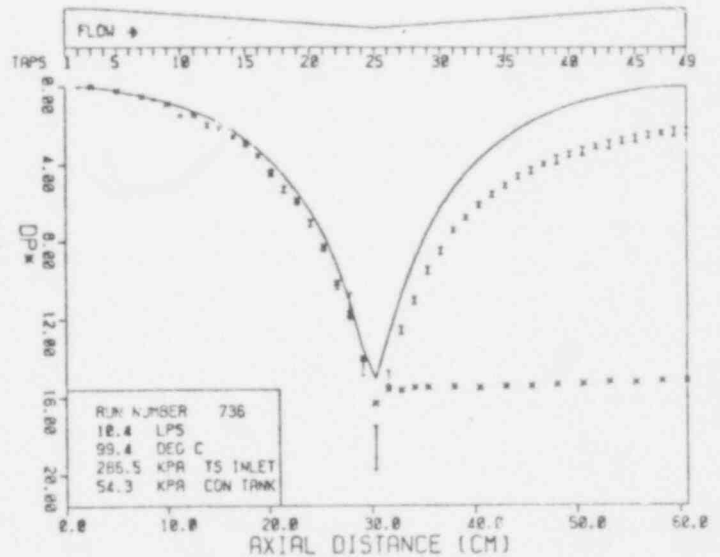
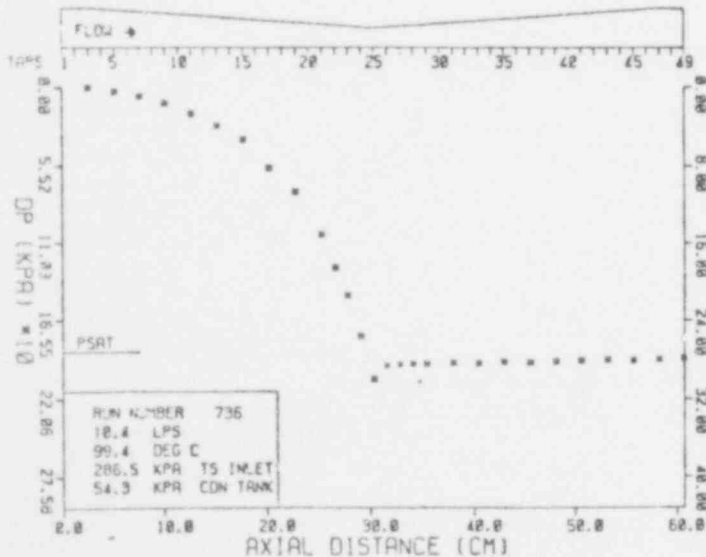


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 736

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-3	10.37	96.3	99.4	88.1	286.4	54.2	510.5	.865E+06	.00	.00
1-5	10.41	96.3	99.4	88.2	286.9	54.4	512.4	.869E+06	2.67	.21
1-7	10.37	96.3	99.4	88.1	286.2	54.5	510.9	.866E+06	6.24	.50
1-9	10.39	96.3	99.4	88.0	287.9	54.5	511.7	.868E+06	11.14	.88
1-11	10.36	96.3	99.3	87.5	285.6	54.6	510.1	.865E+06	18.44	1.47
1-13	10.40	96.3	99.3	87.9	286.6	54.4	512.1	.868E+06	26.77	2.11
1-15	10.38	96.3	99.4	88.3	285.6	54.1	511.1	.867E+06	36.29	2.87
1-17	10.39	96.3	99.4	87.7	285.9	54.3	511.7	.867E+06	56.32	4.45
1-19	10.39	96.3	99.4	87.9	286.6	54.4	511.8	.868E+06	73.28	5.79
1-21	10.37	96.3	99.3	87.6	286.0	54.4	510.8	.866E+06	104.11	8.26
1-22	10.37	96.3	99.4	88.2	287.0	54.1	510.9	.866E+06	128.05	10.15
1-23	10.37	96.3	99.4	88.2	285.4	54.2	510.8	.866E+06	147.91	11.73
1-24	10.37	96.3	99.3	88.2	286.6	54.3	510.5	.865E+06	176.32	14.00
1-25	10.39	96.3	99.4	87.9	286.0	54.3	511.7	.867E+06	206.25	16.30
1-26	10.39	96.3	99.3	87.9	287.1	54.4	511.7	.867E+06	197.02	15.57
1-27	10.35	96.3	99.4	87.8	285.7	54.4	509.9	.864E+06	196.45	15.64
1-28	10.39	96.3	99.4	87.9	285.7	54.4	511.5	.867E+06	195.88	15.49
1-29	10.39	96.3	99.3	88.2	287.9	53.9	511.6	.867E+06	195.89	15.49
1-31	10.38	96.3	99.4	88.1	286.5	54.0	511.3	.867E+06	195.29	15.46
1-33	10.38	96.3	99.4	88.2	286.6	54.1	510.9	.866E+06	195.55	15.51
1-35	10.37	96.3	99.3	88.1	288.2	54.1	510.6	.865E+06	194.52	15.44
1-37	10.39	96.3	99.4	88.2	285.5	54.3	511.4	.867E+06	194.76	15.41
1-39	10.39	96.3	99.4	88.4	286.6	54.3	511.6	.867E+06	194.19	15.36
1-41	10.38	96.3	99.4	87.8	287.2	54.4	511.2	.867E+06	193.54	15.33
1-43	10.40	96.3	99.4	88.1	286.2	54.4	512.1	.869E+06	193.17	15.24
1-45	10.40	96.3	99.4	87.8	286.6	54.5	511.9	.868E+06	193.41	15.28
1-47	10.40	96.3	99.4	87.5	287.0	54.4	512.1	.868E+06	192.65	15.11
1-49	10.39	96.3	99.3	88.0	287.2	54.2	511.9	.868E+06	192.29	15.19
50-1	10.36	96.3	99.4	88.2	285.9	54.2	510.0	.865E+06	17.94	1.43

POOR ORIGINAL

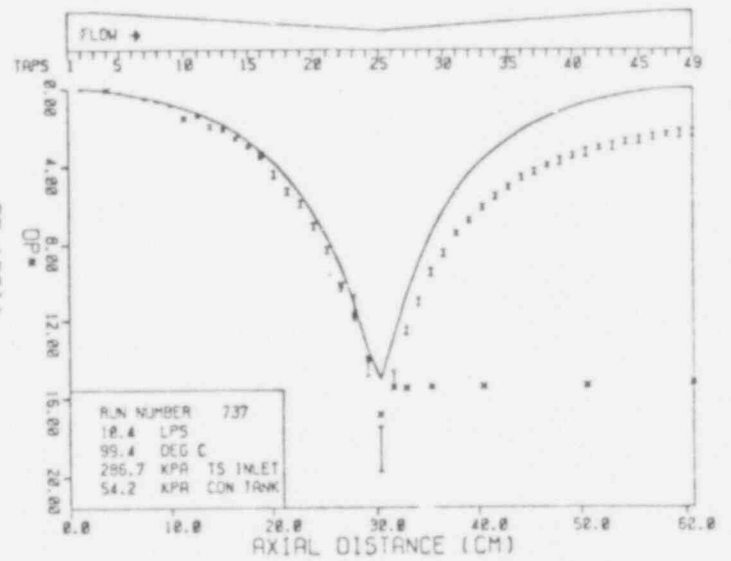
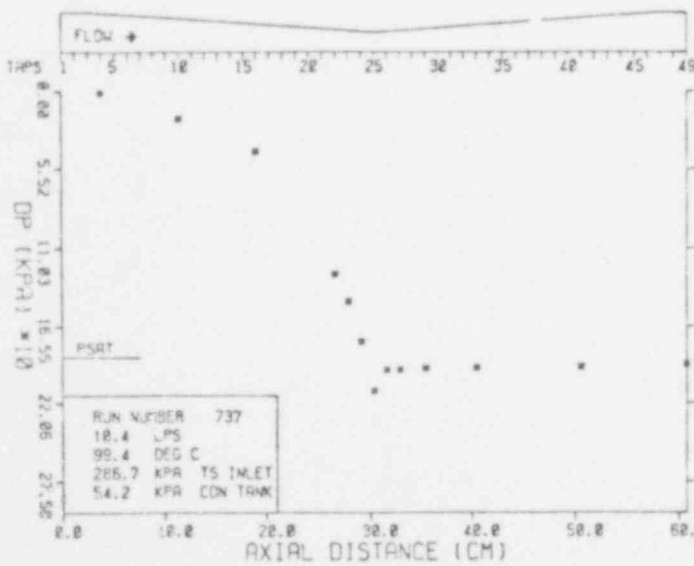


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN # 737

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM/SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLON RETAR	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-4	10.40	99.3	99.4	88.2	285.7	54.8	512.0	.868E+06	.91	.07
1-10	10.39	96.3	99.4	87.8	286.7	54.2	511.5	.867E+06	19.71	1.56
1-16	10.37	96.3	99.4	87.8	287.1	54.2	510.8	.866E+06	42.68	3.39
1-22	10.38	96.3	99.4	87.9	286.5	54.3	510.9	.866E+06	128.13	10.16
1-23	10.36	96.3	99.4	88.3	286.4	53.8	510.0	.865E+06	147.64	11.75
1-24	10.38	96.3	99.4	88.1	287.2	54.0	511.0	.867E+06	176.28	13.97
1-25	10.36	96.3	99.4	87.8	286.0	54.0	509.9	.865E+06	211.83	16.86
1-26	10.41	96.3	99.4	87.8	286.5	54.8	512.4	.869E+06	196.64	15.51
1-27	10.40	96.3	99.4	87.8	287.9	54.2	511.9	.868E+06	196.62	15.53
1-29	10.39	96.3	99.4	87.8	286.1	54.2	511.7	.867E+06	195.62	15.46
1-33	10.39	96.3	99.4	87.9	287.1	54.3	511.5	.867E+06	195.22	15.44
1-41	10.39	96.3	99.4	88.1	287.4	54.3	511.4	.867E+06	194.52	15.39
1-49	10.38	96.3	99.4	87.8	286.7	54.3	510.9	.866E+06	192.15	15.23
50-1	10.39	96.3	99.4	87.8	287.3	54.4	511.7	.868E+06	18.02	1.42

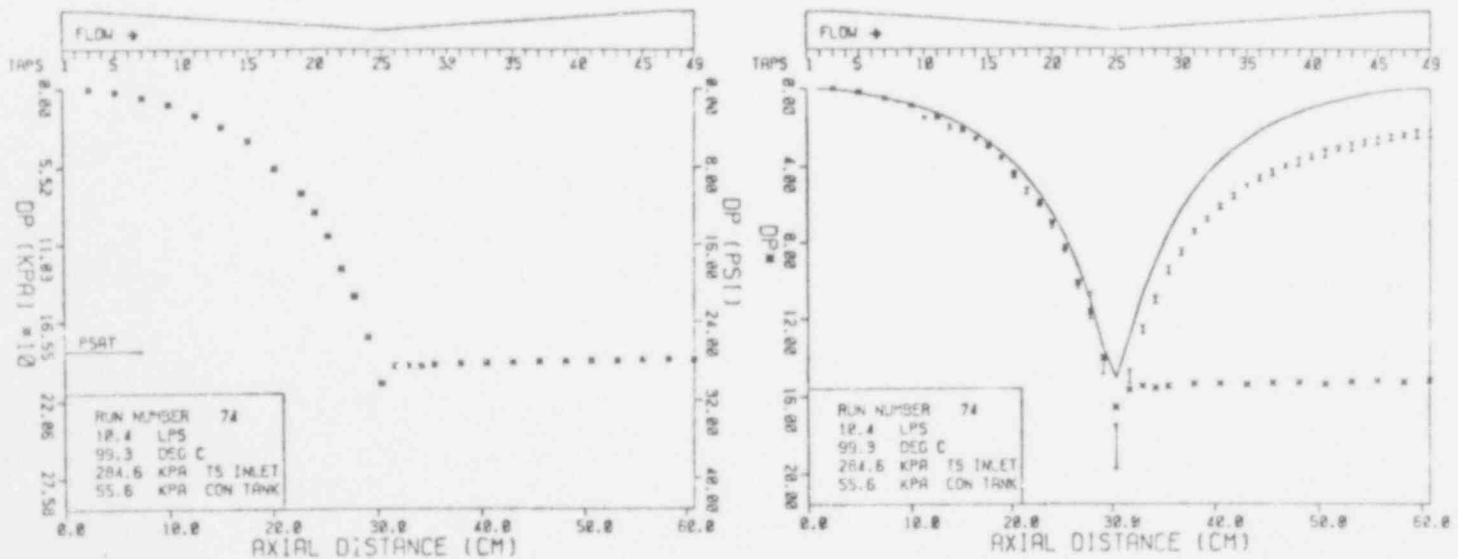
**POOR ORIGINAL**



BNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-3	10.36	96.3	99.3	87.9	285.9	55.5	510.4	.865E+06	.00	.00
1-5	10.35	96.3	99.3	87.9	284.7	55.5	509.8	.864E+06	2.38	.19
1-7	10.39	96.3	99.4	88.0	284.5	55.4	511.6	.867E+06	6.21	.49
1-9	10.37	96.3	99.3	87.8	283.8	55.4	510.6	.866E+06	10.95	.87
1-11	10.39	96.3	99.3	87.8	284.6	55.5	511.4	.867E+06	18.39	1.45
1-13	10.36	96.3	99.4	87.9	284.8	55.5	510.3	.865E+06	26.64	2.12
1-15	10.38	96.3	99.3	87.9	284.7	55.5	511.2	.866E+06	36.44	2.89
1-17	10.37	96.3	99.4	87.7	284.0	55.5	510.7	.866E+06	56.23	4.46
1-19	10.36	96.3	99.4	87.6	283.8	55.6	510.1	.865E+06	73.37	5.84
1-21	10.36	96.3	99.4	87.9	284.2	55.6	510.1	.865E+06	87.11	6.93
1-21	10.39	96.3	99.3	87.8	284.4	55.6	511.5	.867E+06	104.25	8.25
1-23	10.36	96.3	99.3	87.9	284.6	55.6	510.3	.865E+06	127.88	10.16
1-23	10.39	96.3	99.3	87.8	285.2	55.6	511.3	.867E+06	147.31	11.66
1-24	10.36	96.3	99.3	87.8	284.0	55.6	510.3	.865E+06	176.15	14.00
1-25	10.36	96.3	99.4	87.6	283.5	55.6	510.0	.865E+06	208.24	16.57
1-29	10.34	96.3	99.3	87.6	284.8	55.8	509.2	.863E+06	196.18	15.66
1-27	10.39	96.3	99.3	87.9	285.4	55.8	511.5	.867E+06	195.73	15.48
1-26	10.37	96.3	99.3	87.8	285.5	55.7	510.5	.865E+06	196.05	15.57
1-29	10.37	96.3	99.3	87.8	285.8	55.8	510.7	.866E+06	195.34	15.50
1-31	10.39	96.3	99.3	87.7	283.8	55.8	511.7	.867E+06	194.48	15.37
1-35	10.39	96.3	99.3	87.9	284.0	55.7	511.4	.867E+06	194.10	15.36
1-35	10.35	96.3	99.3	88.0	284.8	55.7	509.9	.864E+06	193.55	15.41
1-37	10.38	96.3	99.3	88.2	285.2	55.7	511.0	.866E+06	193.37	15.33
1-29	10.38	96.3	99.4	88.1	285.7	55.7	510.9	.866E+06	192.95	15.30
1-41	10.34	96.3	99.3	87.8	284.0	55.7	509.4	.863E+06	192.72	15.27
1-43	10.39	96.3	99.3	87.8	284.4	55.7	511.1	.866E+06	192.72	15.27
1-45	10.38	96.3	99.3	88.1	284.6	55.7	511.2	.866E+06	191.99	15.20
1-47	10.35	96.3	99.3	87.8	283.6	55.8	509.7	.864E+06	191.92	15.29
1-49	10.39	96.3	99.3	88.2	284.6	55.7	511.6	.867E+06	192.15	15.19
50-1	10.37	96.3	99.3	88.1	284.5	55.5	510.5	.865E+06	17.94	1.42

POOR ORIGINAL

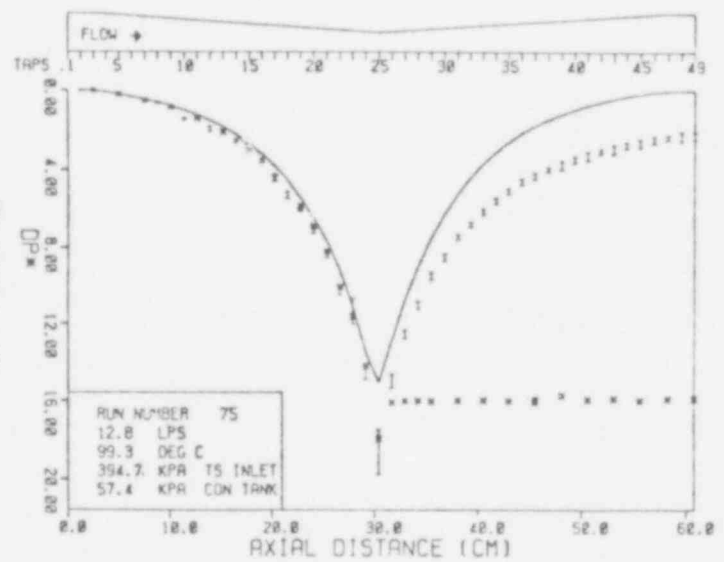
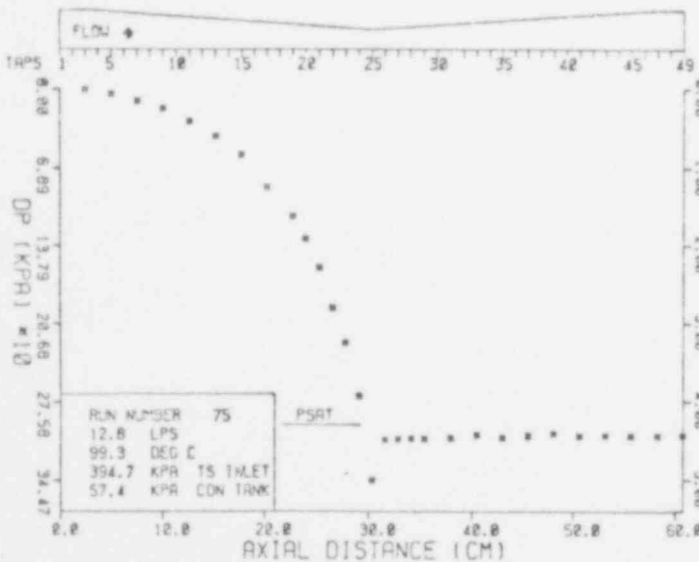


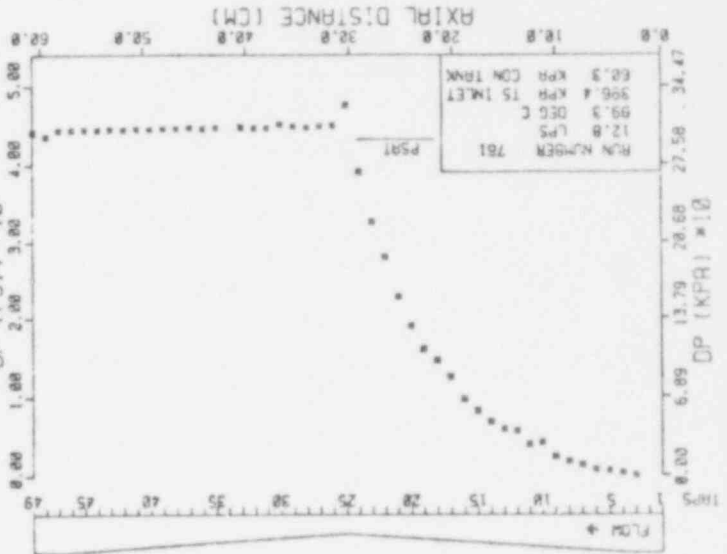
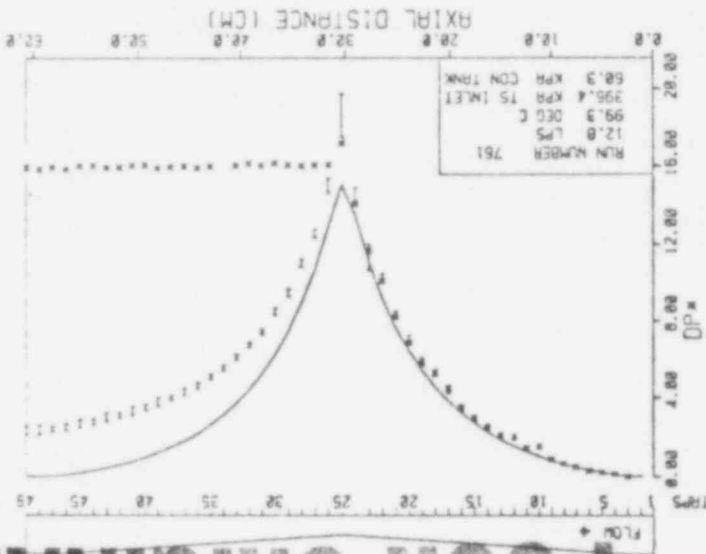
BNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER 75

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW ENTER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-3	12.76	96.9	99.3	88.1	395.2	57.2	628.5	.106E+07	.49	.03
1-5	12.78	96.9	99.3	88.3	391.7	57.2	629.3	.107E+07	4.17	.22
1-7	12.81	96.9	99.3	88.2	392.5	57.3	630.7	.107E+07	10.23	.53
1-9	12.82	96.9	99.3	88.5	394.7	57.3	631.1	.107E+07	16.63	.86
1-11	12.82	96.9	99.3	88.3	394.8	57.3	631.4	.107E+07	27.87	1.45
1-13	12.78	96.9	99.3	88.4	394.5	57.3	629.2	.107E+07	40.78	2.13
1-15	12.81	96.9	99.3	88.3	394.1	57.4	630.7	.107E+07	56.72	2.95
1-17	12.82	96.9	99.3	88.2	396.0	57.2	631.1	.107E+07	85.53	4.44
1-19	12.79	96.9	99.3	88.5	394.6	57.3	629.6	.107E+07	111.27	5.81
1-20	12.80	96.9	99.4	88.5	393.5	57.3	630.5	.107E+07	131.59	6.85
1-21	12.81	96.9	99.3	88.3	394.9	57.4	630.7	.107E+07	157.13	8.17
1-22	12.80	96.9	99.4	88.3	395.6	57.4	630.2	.107E+07	192.92	10.05
1-23	12.81	96.9	99.3	88.5	392.6	57.4	631.0	.107E+07	223.75	11.63
1-24	12.75	96.9	99.3	88.4	395.1	57.2	627.8	.106E+07	270.29	14.19
1-25	12.81	96.9	99.3	88.6	394.6	57.4	630.7	.107E+07	344.37	17.91
1-26	12.79	96.9	99.3	88.8	393.4	57.3	630.0	.107E+07	308.91	16.10
1-27	12.81	96.9	99.3	88.7	395.3	57.3	630.9	.107E+07	308.12	16.02
1-28	12.81	96.9	99.3	88.4	395.9	57.4	630.8	.107E+07	308.02	16.02
1-29	12.79	96.9	99.3	88.4	396.9	57.5	629.9	.107E+07	307.74	16.05
1-31	12.80	96.9	99.3	88.7	394.8	57.5	630.3	.107E+07	307.37	16.01
1-33	12.76	96.9	99.3	88.7	396.2	57.5	628.5	.107E+07	305.24	15.99
1-35	12.80	96.9	99.3	88.8	394.5	57.5	630.2	.107E+07	307.46	16.02
1-37	12.80	96.9	99.3	88.6	395.1	57.4	630.2	.107E+07	305.49	15.92
1-39	12.76	96.9	99.4	88.4	395.0	57.4	628.4	.107E+07	306.99	16.09
1-41	12.83	96.9	99.3	88.3	395.4	57.4	631.6	.107E+07	303.67	15.75
1-43	12.81	96.9	99.3	88.3	394.7	57.5	630.6	.107E+07	306.29	15.94
1-45	12.81	96.9	99.3	88.3	396.0	57.6	630.6	.107E+07	305.44	15.89
1-47	12.77	96.9	99.3	88.3	394.8	57.6	628.7	.107E+07	305.74	16.00
1-49	12.80	96.9	99.3	88.5	394.2	57.5	630.2	.107E+07	305.72	15.93
1-49	12.80	96.9	99.3	88.2	394.8	57.5	630.5	.107E+07	305.29	15.89
50-1	12.79	96.9	99.3	89.0	394.8	57.6	629.8	.107E+07	27.92	1.46

**POOR ORIGINAL**



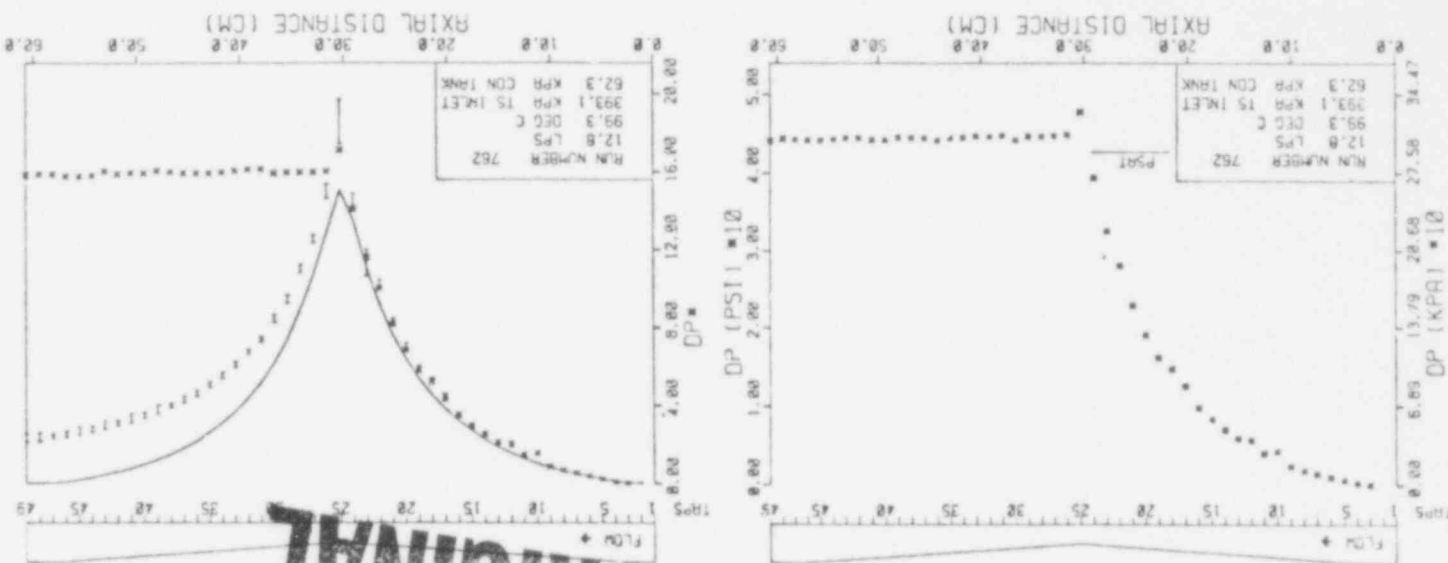


**POOR ORIGINAL**

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)	TEMPERATURE (KPA)	VELOCITY	MEASURED DIFFERENTIAL PRESSURE
1-3	12.84	99.3	99.3	632.2	0.0
1-4	12.81	99.3	99.3	630.2	1.1
1-5	12.81	99.3	99.3	630.8	2.3
1-6	12.80	99.3	99.3	630.4	5.6
1-7	12.78	99.3	99.3	629.1	9.5
1-8	12.78	99.3	99.3	629.5	12.6
1-9	12.83	99.3	99.3	631.6	16.7
1-10	12.79	99.3	99.3	629.3	29.3
1-11	12.80	99.3	99.3	630.3	27.7
1-12	12.83	99.3	99.3	631.6	39.2
1-13	12.80	99.3	99.3	630.5	40.8
1-14	12.76	99.3	99.3	628.4	47.6
1-15	12.78	99.3	99.3	629.3	57.0
1-16	12.82	99.3	99.3	631.5	66.8
1-17	12.80	99.3	99.3	630.5	86.0
1-18	12.82	99.3	99.3	631.3	101.0
1-19	12.87	99.3	99.3	631.3	110.5
1-20	12.84	99.3	99.3	629.5	130.8
1-21	12.79	99.3	99.3	629.7	157.0
1-22	12.78	99.3	99.3	629.4	193.1
1-23	12.80	99.3	99.3	630.2	224.3
1-24	12.77	99.3	99.3	628.8	259.0
1-25	12.76	99.3	99.3	628.5	327.6
1-26	12.83	99.3	99.3	631.7	319.7
1-27	12.82	99.3	99.3	631.5	308.9
1-28	12.81	99.3	99.3	630.8	309.0
1-29	12.81	99.3	99.3	630.9	316.5
1-30	12.81	99.3	99.3	630.9	307.9
1-31	12.81	99.3	99.3	630.5	307.6
1-32	12.76	99.3	99.3	628.4	308.1
1-33	12.80	99.3	99.3	630.5	307.3
1-34	12.83	99.3	99.3	630.7	306.9
1-35	12.83	99.3	99.3	631.8	306.9
1-36	12.83	99.3	99.3	630.7	307.4
1-37	12.82	99.3	99.3	630.7	307.4
1-38	12.87	99.3	99.3	631.1	307.2
1-39	12.87	99.3	99.3	632.0	306.7
1-40	12.77	99.3	99.3	628.0	306.7
1-41	12.77	99.3	99.3	628.8	306.4
1-42	12.81	99.3	99.3	629.4	306.7
1-43	12.81	99.3	99.3	630.2	306.1
1-44	12.78	99.3	99.3	629.4	306.7
1-45	12.78	99.3	99.3	628.8	306.4
1-46	12.78	99.3	99.3	629.5	306.2
1-47	12.79	99.3	99.3	629.7	306.2
1-48	12.74	99.3	99.3	627.1	304.5
1-49	12.78	99.3	99.3	629.3	304.5
50-1	12.78	99.3	99.3	629.5	28.0

BNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2  
RUN NUMBER 761

575 201



POOR ORIGINAL

BML FLASHING FLOW EXPERIMENT

PRESSURE DROP DATA FROM

TEST SECTION # 2

RUN NUMBER 762

TAPS	LOOP FLOW	TEMPERATURES (DBO C)	FLOW METER TS INLET COND TANK	TS INLET COND TANK	PRESSURE (KPA)	VELOCITY	REYNOLDS	DIFFERENTIAL PRESSURE
1-3	12.82	99.3	88.1	93.9	933.9	61.9	631.5	1.69
1-4	12.83	99.3	88.1	94.0	934.0	62.0	631.5	1.69
1-5	12.84	99.3	88.2	94.0	934.0	62.0	631.5	1.69
1-6	12.84	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-7	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-8	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-9	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-10	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-11	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-12	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-13	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-14	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-15	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-16	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-17	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-18	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-19	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-20	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-21	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-22	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-23	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-24	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-25	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-26	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-27	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-28	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-29	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-30	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-31	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-32	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-33	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-34	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-35	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-36	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-37	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-38	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-39	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-40	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-41	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-42	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-43	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-44	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-45	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-46	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-47	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-48	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-49	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69
1-50	12.85	99.3	88.2	94.1	934.1	62.1	631.5	1.69



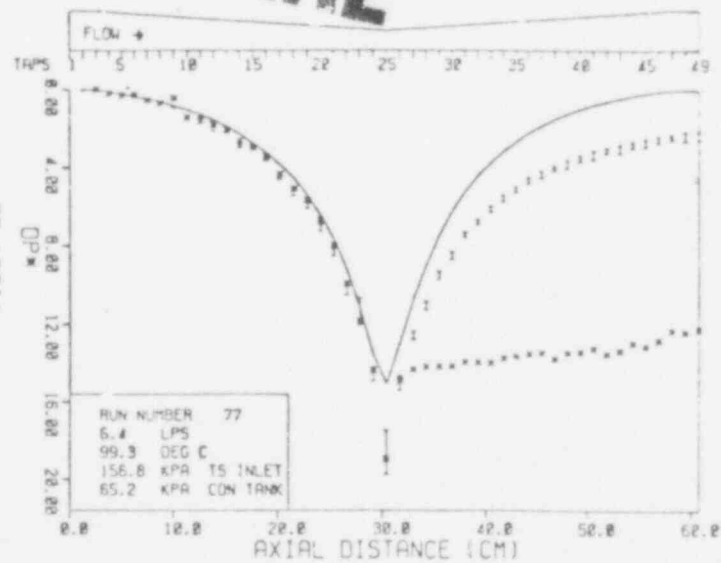
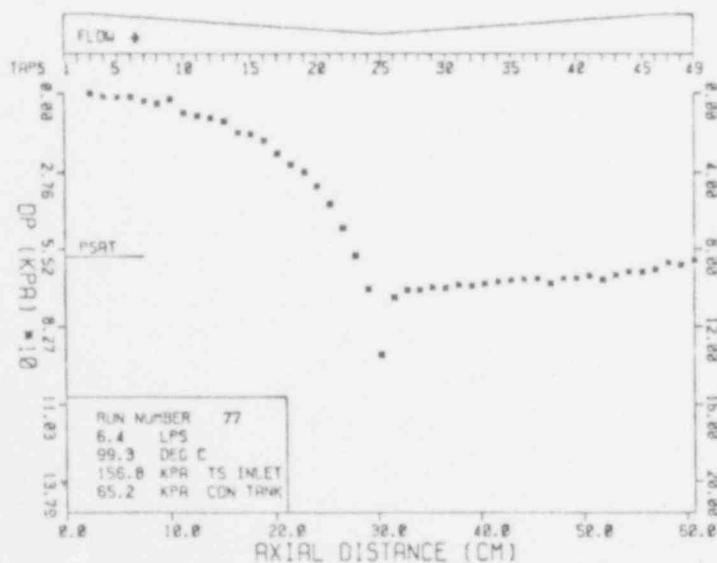


BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 77

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM/SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-3	6.43	93.5	99.3	88.6	159.6	65.0	316.8	532E+06	.00	.00
1-4	6.39	93.6	99.4	88.9	159.0	65.0	314.7	534E+06	.96	.70
1-5	6.43	93.5	99.3	88.9	157.0	65.0	316.7	532E+06	1.41	.79
1-6	6.42	93.6	99.3	88.6	158.5	64.9	316.0	535E+06	1.22	.75
1-7	6.44	93.6	99.3	88.6	159.6	65.0	317.3	538E+06	2.67	.55
1-8	6.41	93.6	99.3	88.7	158.0	65.0	315.5	535E+06	3.41	.71
1-9	6.44	93.6	99.3	89.0	158.6	65.0	317.1	538E+06	2.14	.44
1-10	6.42	93.6	99.3	88.8	159.1	65.0	316.2	530E+06	6.81	1.41
1-11	6.42	93.6	99.3	88.6	159.1	65.1	316.0	536E+06	7.72	1.60
1-12	6.39	93.6	99.3	89.0	158.4	65.0	314.7	533E+06	8.56	1.79
1-13	6.42	93.6	99.3	88.5	158.5	65.1	316.3	536E+06	9.70	2.01
1-14	6.40	93.5	99.3	88.9	159.4	65.1	315.4	535E+06	13.70	2.85
1-15	6.42	93.6	99.3	88.7	158.8	65.1	316.4	536E+06	14.26	2.95
1-16	6.45	93.6	99.4	88.6	158.0	65.2	317.5	538E+06	16.62	3.41
1-17	6.43	93.6	99.4	88.5	158.4	65.2	316.5	537E+06	21.00	4.34
1-18	6.45	93.6	99.3	88.6	158.9	65.2	317.5	538E+06	24.79	5.09
1-19	6.41	93.6	99.3	88.5	158.3	65.3	315.8	535E+06	27.28	5.66
1-20	6.43	93.6	99.3	88.5	158.8	65.2	316.7	537E+06	32.38	6.68
1-21	6.45	93.6	99.3	88.8	158.7	65.3	317.4	538E+06	38.81	7.97
1-22	6.40	93.6	99.3	88.5	158.7	65.3	315.1	534E+06	47.57	9.91
1-23	6.44	93.6	99.3	88.9	157.9	65.2	317.2	538E+06	57.52	11.83
1-24	6.42	93.6	99.3	88.8	157.9	65.3	316.0	536E+06	69.31	14.37
1-25	6.46	93.6	99.3	89.0	155.4	65.3	318.0	539E+06	92.64	18.95
1-26	6.43	93.6	99.3	88.9	156.0	65.2	316.8	537E+06	72.38	14.93
1-27	6.45	93.6	99.3	89.2	155.4	65.3	317.8	539E+06	69.82	14.31
1-28	6.48	93.6	99.3	88.7	154.9	65.3	319.0	541E+06	69.64	14.17
1-29	6.44	93.6	99.3	88.7	154.7	65.3	317.1	538E+06	68.67	14.14
1-30	6.45	93.6	99.3	88.5	155.7	65.2	317.6	538E+06	68.93	14.14
1-31	6.45	93.6	99.3	88.8	154.8	65.2	317.8	538E+06	67.89	13.91
1-32	6.46	93.6	99.3	88.6	155.4	65.3	317.9	539E+06	68.06	13.94
1-33	6.42	93.6	99.3	89.0	155.2	65.3	316.1	536E+06	67.37	13.85
1-34	6.45	93.6	99.3	88.7	155.2	65.2	317.4	538E+06	66.78	13.72
1-35	6.45	93.6	99.3	88.8	155.2	65.2	317.9	539E+06	65.90	13.59
1-36	6.46	93.6	99.3	88.8	155.6	65.1	317.9	539E+06	65.79	13.45
1-37	6.46	93.5	99.3	88.6	155.0	65.2	318.2	539E+06	67.26	13.76
1-38	6.46	93.5	99.3	88.8	155.2	65.2	318.1	539E+06	65.69	13.46
1-39	6.46	93.6	99.4	88.7	155.0	65.3	317.9	539E+06	65.69	13.46
1-40	6.45	93.6	99.3	88.7	154.5	65.3	317.6	538E+06	65.37	13.41
1-41	6.45	93.6	99.3	88.8	155.1	65.3	317.8	539E+06	64.67	13.25
1-42	6.45	93.6	99.3	88.3	155.4	65.3	317.7	538E+06	65.94	13.52
1-43	6.41	93.6	99.3	88.4	155.2	65.3	315.9	535E+06	64.29	13.34
1-44	6.45	93.6	99.3	88.6	155.7	65.4	317.8	539E+06	63.72	12.96
1-45	6.42	93.6	99.3	88.8	155.3	65.4	316.2	536E+06	63.31	12.89
1-46	6.45	93.5	99.3	88.9	155.3	65.4	317.4	538E+06	60.04	12.30
1-47	6.45	93.6	99.3	88.9	155.2	65.3	317.8	538E+06	60.65	12.38
1-48	6.47	93.5	99.3	88.9	154.7	65.4	318.4	540E+06	59.15	12.23
1-49	6.42	93.5	99.3	88.8	155.8	65.5	316.4	536E+06	6.15	1.25
50-1	6.47	93.5	99.3	88.8	155.5	65.4	318.6	540E+06		

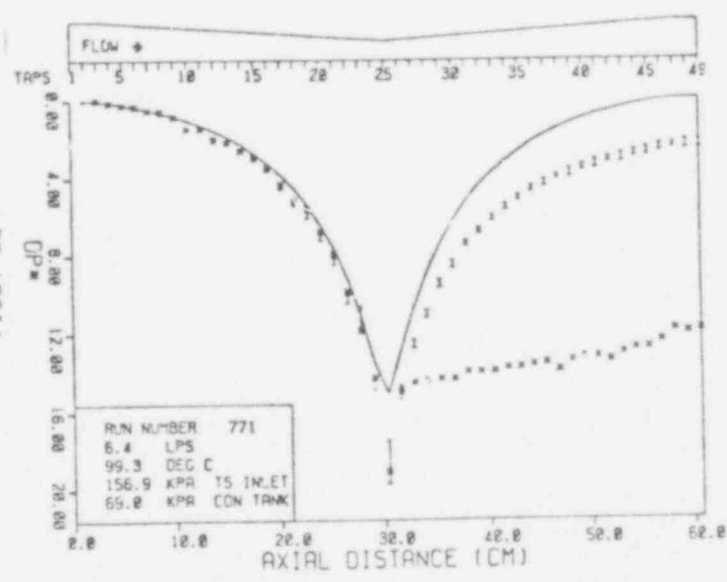
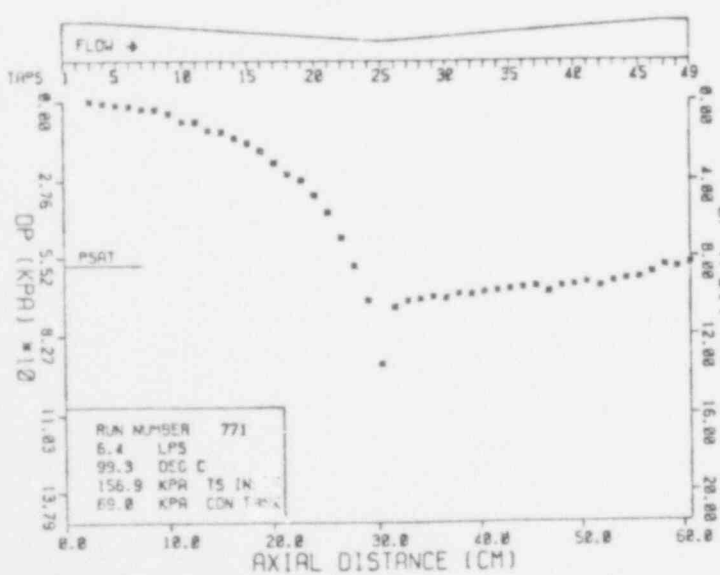
POOR ORIGINAL



# POOR ORIC

## BNL FLASHING FLOWS EXPERIMENT PRESSURE DROP DATA FROM TEST SECTION # 2

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-3	6.44	93.6	99.3	87.9	156.8	68.8	317.0	.537E+06	.00	.00
1-4	6.41	93.6	99.3	87.9	157.5	68.9	315.8	.535E+06	.68	.14
1-5	6.43	93.6	99.3	88.0	156.4	68.9	316.6	.537E+06	1.22	.25
1-6	6.45	93.6	99.3	88.1	156.8	68.8	317.8	.539E+06	1.59	.33
1-7	6.45	93.6	99.3	88.1	156.3	68.8	317.7	.538E+06	2.51	.52
1-8	6.44	93.6	99.3	88.1	156.8	69.0	317.3	.538E+06	2.75	.57
1-9	6.45	93.6	99.4	88.2	157.6	69.0	317.5	.538E+06	4.09	.84
1-10	6.43	93.6	99.3	88.3	157.0	68.9	316.5	.537E+06	7.09	1.46
1-11	6.43	93.6	99.4	88.1	156.6	69.0	316.6	.537E+06	6.98	1.44
1-12	6.44	93.6	99.3	88.0	156.4	69.0	317.2	.538E+06	9.96	2.05
1-13	6.42	93.6	99.4	88.9	157.2	68.9	315.9	.536E+06	10.40	2.16
1-14	6.43	93.6	99.3	88.7	157.0	68.9	316.6	.537E+06	12.51	2.58
1-15	6.45	93.6	99.3	88.5	156.9	68.9	317.6	.538E+06	14.27	2.93
1-16	6.42	93.6	99.3	88.2	157.1	68.9	316.3	.536E+06	16.78	3.47
1-17	6.45	93.6	99.3	88.4	156.3	68.9	317.8	.539E+06	21.23	4.35
1-18	6.44	93.6	99.3	88.4	157.0	68.9	316.9	.537E+06	25.06	5.16
1-19	6.46	93.6	99.3	88.3	156.6	68.9	318.2	.539E+06	27.37	5.60
1-20	6.43	93.6	99.3	87.9	155.9	68.9	316.4	.536E+06	32.69	6.76
1-21	6.46	93.6	99.3	88.3	157.3	68.9	318.1	.539E+06	38.94	7.96
1-22	6.44	93.6	99.3	88.2	157.1	69.0	317.1	.537E+06	47.99	9.88
1-23	6.45	93.6	99.3	88.6	156.6	69.0	317.8	.539E+06	58.01	11.88
1-24	6.48	93.6	99.4	88.4	157.7	69.1	319.0	.541E+06	70.27	14.29
1-25	6.43	93.6	99.3	88.1	156.6	69.0	316.8	.537E+06	92.46	19.07
1-26	6.44	93.6	99.3	88.1	156.5	69.1	317.0	.537E+06	72.67	14.97
1-27	6.44	93.6	99.3	88.2	156.8	69.1	317.0	.537E+06	70.41	14.50
1-28	6.44	93.6	99.3	88.3	156.7	69.0	316.9	.537E+06	69.87	14.39
1-29	6.42	93.6	99.4	88.1	157.3	69.1	315.9	.536E+06	69.07	14.32
1-30	6.44	93.6	99.3	88.2	157.5	69.1	317.0	.537E+06	69.50	14.32
1-31	6.45	93.6	99.3	88.2	157.2	69.1	317.4	.538E+06	68.08	13.98
1-32	6.46	93.6	99.4	88.0	157.2	69.1	317.9	.539E+06	68.31	13.99
1-33	6.42	93.6	99.3	88.3	156.5	69.1	316.0	.536E+06	67.41	13.97
1-34	6.44	93.6	99.3	88.1	157.1	69.1	317.0	.537E+06	67.03	13.80
1-35	6.42	93.6	99.3	88.0	157.3	69.1	316.1	.536E+06	66.46	13.77
1-36	6.43	93.6	99.4	88.1	156.5	69.1	316.9	.537E+06	66.08	13.65
1-37	6.43	93.6	99.3	88.3	156.6	69.1	316.9	.537E+06	65.66	13.54
1-38	6.44	93.6	99.4	88.2	156.6	69.1	317.1	.538E+06	67.55	13.90
1-39	6.45	93.6	99.3	88.4	156.6	69.1	317.6	.538E+06	65.46	13.43
1-40	6.48	93.6	99.4	88.0	157.0	69.1	319.1	.541E+06	65.12	13.24
1-41	6.44	93.6	99.3	88.1	157.7	69.1	316.9	.537E+06	64.23	13.24
1-42	6.46	93.6	99.3	88.2	155.8	69.0	318.0	.539E+06	65.55	13.42
1-43	6.46	93.6	99.3	88.6	157.0	69.0	318.1	.539E+06	63.84	13.06
1-44	6.47	93.6	99.3	88.6	156.5	69.0	318.5	.540E+06	62.99	12.85
1-45	6.45	93.6	99.3	88.6	156.8	69.0	317.8	.539E+06	62.50	12.81
1-46	6.45	93.6	99.3	88.3	156.8	69.0	317.5	.538E+06	60.72	12.46
1-47	6.47	93.6	99.3	88.4	157.0	69.0	318.4	.540E+06	58.26	11.89
1-48	6.47	93.6	99.3	88.2	156.6	69.0	318.4	.540E+06	58.95	12.03
1-49	6.42	93.6	99.3	88.3	157.1	69.1	316.0	.536E+06	57.37	11.89
50-1	6.42	93.6	99.4	88.7	157.3	69.1	316.1	.536E+06	5.05	1.05
1-13	6.45	93.5	99.3	88.2	157.2	69.2	317.5	.538E+06	.96	.20



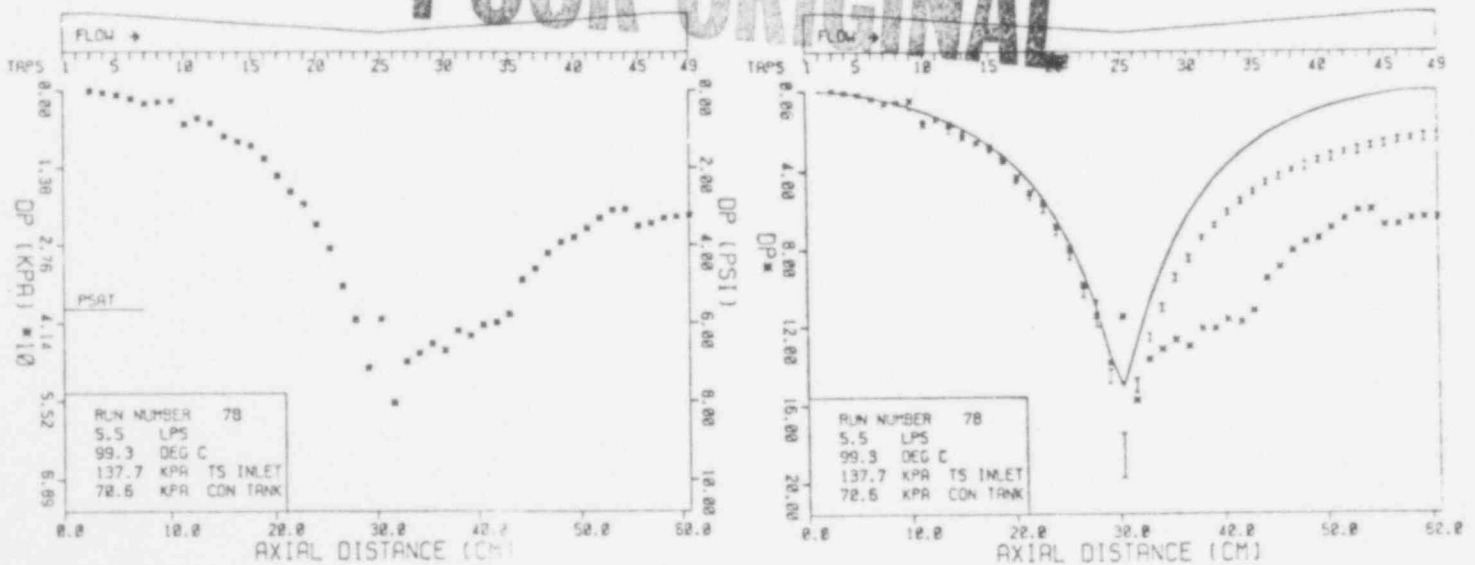
575 204

BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

RUN NUMBER 78

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-3	5.47	92.3	99.5	87.9	138.1	70.7	269.4	.457E+06	.00	.00
1-4	5.49	92.3	99.3	88.1	136.8	70.5	270.3	.458E+06	.25	.10
1-5	5.51	92.3	99.2	87.8	136.8	70.4	271.6	.460E+06	.75	.21
1-6	5.51	92.3	99.2	88.1	137.1	70.3	271.5	.460E+06	1.44	.41
1-7	5.48	92.3	99.4	87.8	138.5	70.6	270.1	.458E+06	2.28	.65
1-8	5.49	92.3	99.4	88.1	138.4	70.4	270.3	.459E+06	2.03	.59
1-9	5.53	92.3	99.2	87.9	137.5	70.2	272.3	.461E+06	1.81	.51
1-10	5.52	92.3	99.2	87.8	137.1	70.3	271.6	.460E+06	5.93	1.66
1-11	5.49	92.3	99.5	87.9	138.9	70.6	270.4	.459E+06	4.94	1.40
1-12	5.50	92.3	99.5	87.9	138.4	70.6	270.9	.460E+06	5.81	1.64
1-13	5.49	92.3	99.3	87.7	137.7	70.3	270.4	.458E+06	8.18	2.32
1-14	5.49	92.3	99.1	87.7	137.0	70.2	270.3	.457E+06	9.14	2.59
1-15	5.50	92.3	99.4	88.0	138.3	70.7	270.8	.460E+06	9.88	2.79
1-16	5.48	92.3	99.6	88.2	139.0	70.6	269.8	.458E+06	12.24	3.48
1-17	5.50	92.3	99.2	88.0	137.3	70.2	270.7	.458E+06	15.27	4.31
1-18	5.51	92.3	99.1	87.8	136.5	70.3	271.6	.459E+06	18.08	5.17
1-19	5.54	92.3	99.2	88.1	136.7	70.5	272.6	.462E+06	20.25	5.64
1-20	5.48	92.3	99.6	87.7	138.8	70.9	269.9	.459E+06	23.94	6.90
1-21	5.51	92.3	99.5	87.6	139.3	70.6	271.2	.460E+06	28.22	7.94
1-22	5.50	92.3	99.2	87.7	136.9	70.3	270.8	.459E+06	34.81	9.82
1-23	5.51	92.3	99.2	87.9	136.1	70.6	271.2	.459E+06	40.68	11.45
1-24	5.51	92.3	99.4	87.9	137.4	70.7	271.1	.460E+06	49.24	13.95
1-25	5.50	92.3	99.5	87.7	138.1	70.7	270.8	.460E+06	49.69	13.98
1-26	5.48	92.3	99.3	87.9	137.5	70.5	269.7	.457E+06	55.41	15.76
1-27	5.48	92.3	99.2	87.8	136.7	70.5	269.9	.457E+06	48.17	13.69
1-28	5.50	92.3	99.3	87.9	137.2	70.6	270.7	.459E+06	46.70	13.19
1-29	5.50	92.3	99.5	87.8	138.3	70.8	270.7	.460E+06	45.00	12.83
1-30	5.50	92.3	99.4	88.1	138.6	70.5	270.9	.460E+06	46.20	13.03
1-31	5.48	92.3	99.2	88.3	137.0	70.3	270.8	.457E+06	47.77	13.14
1-32	5.54	92.3	99.1	88.0	136.4	70.4	272.6	.461E+06	43.59	12.14
1-33	5.52	92.3	99.2	88.3	137.0	70.6	271.8	.460E+06	41.70	11.68
1-34	5.47	92.3	99.4	88.0	138.4	70.9	269.2	.457E+06	41.31	11.80
1-35	5.50	92.3	99.5	88.3	138.9	70.8	270.8	.460E+06	39.76	11.22
1-36	5.48	92.3	99.3	87.8	137.4	70.5	270.0	.457E+06	33.72	9.57
1-37	5.51	92.3	99.3	88.0	137.4	70.9	271.2	.460E+06	31.77	8.94
1-38	5.53	92.3	99.4	87.8	138.4	71.0	272.3	.462E+06	28.92	8.07
1-39	5.50	92.3	99.2	87.5	137.3	70.9	271.0	.459E+06	27.02	7.61
1-40	5.49	92.3	99.4	87.6	138.2	71.1	270.1	.458E+06	26.23	7.44
1-41	5.51	92.3	99.3	88.0	137.1	70.6	271.4	.460E+06	24.53	6.89
1-42	5.49	92.3	99.2	87.6	137.3	70.9	270.3	.458E+06	22.75	6.44
1-43	5.50	92.3	99.2	87.9	137.1	70.9	270.6	.458E+06	21.31	6.02
1-44	5.49	92.3	99.1	88.2	136.1	70.6	270.6	.458E+06	21.15	5.98
1-45	5.51	92.3	99.3	88.2	137.7	71.1	271.5	.460E+06	24.12	6.78
1-46	5.48	92.3	99.5	88.3	139.9	71.0	270.0	.459E+06	23.74	6.74
1-47	5.50	92.3	99.4	88.1	138.4	70.8	270.8	.459E+06	22.81	6.44
1-48	5.50	92.3	99.2	87.9	136.8	70.7	270.6	.458E+06	22.55	6.37
1-49	5.47	92.3	99.4	89.5	138.3	70.6	269.3	.457E+06	22.30	6.26
50-1	5.48	92.3	99.6	88.3	140.1	71.2	270.1	.459E+06	2.47	.70

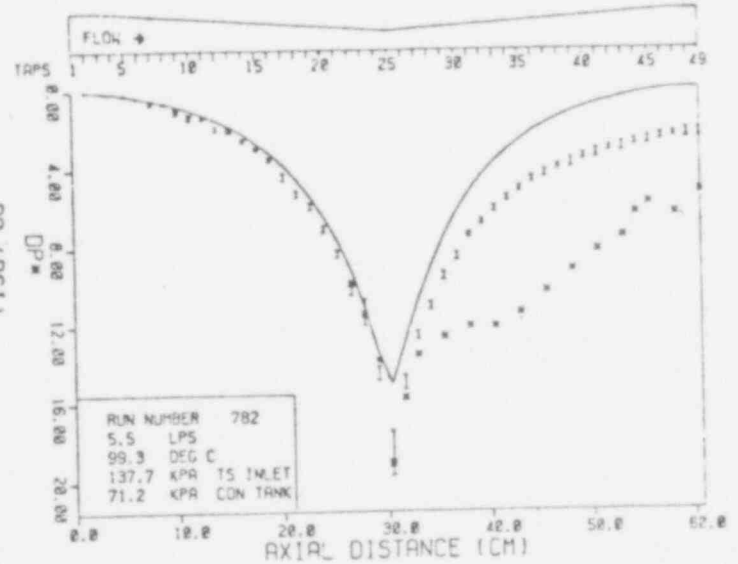
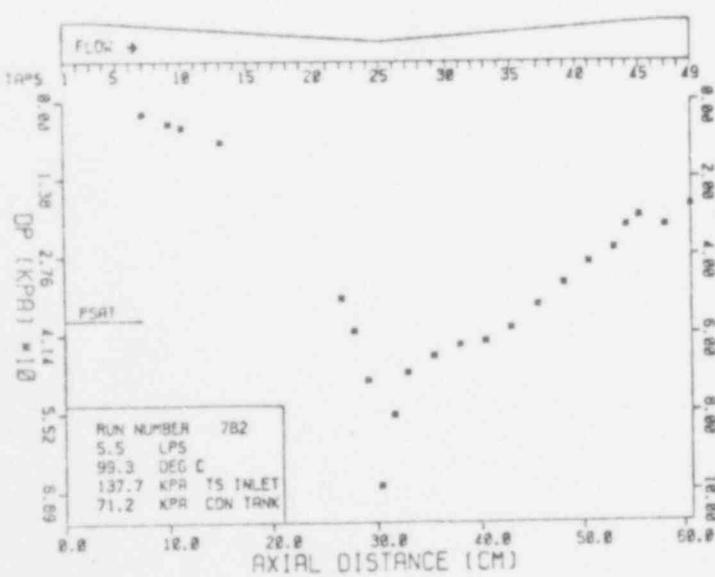
POOR ORIGINAL



BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-7	5.50	92.4	99.2	88.5	136.8	71.0	270.8	.459E+06	2.19	.62
1-9	5.47	92.3	99.5	88.3	138.1	71.3	269.5	.458E+06	3.90	1.11
1-10	5.51	92.3	99.4	87.9	137.9	71.1	271.4	.451E+06	4.59	1.29
1-13	5.51	92.3	99.4	88.0	137.4	71.3	271.1	.460E+06	7.18	2.02
1-22	5.51	92.3	99.3	87.8	137.5	71.0	271.2	.460E+06	34.89	9.82
1-23	5.50	92.4	99.3	88.1	137.1	71.2	270.9	.459E+06	40.68	11.47
1-24	5.51	92.3	99.3	88.1	137.4	71.3	271.4	.460E+06	49.30	13.86
1-25	5.50	92.3	99.5	88.2	138.9	71.4	270.7	.460E+06	67.99	19.18
1-25	5.52	92.3	99.2	88.2	139.4	70.8	271.6	.460E+06	67.94	19.06
1-26	5.48	92.3	99.1	88.3	136.3	70.9	269.9	.457E+06	55.59	15.79
1-27	5.50	92.3	99.6	88.1	138.9	71.5	270.7	.460E+06	48.03	13.57
1-29	5.53	92.3	99.2	87.9	137.0	70.9	272.2	.461E+06	45.19	12.62
1-31	5.52	92.3	99.1	87.9	135.9	71.1	271.9	.460E+06	43.16	12.05
1-33	5.48	92.3	99.6	88.3	139.3	71.6	270.1	.459E+06	42.57	12.08
1-35	5.49	92.3	99.2	88.2	136.4	70.8	270.3	.458E+06	40.26	11.40
1-37	5.48	92.4	99.3	88.0	137.2	70.9	269.8	.457E+06	36.17	10.28
1-39	5.49	92.3	99.6	87.9	139.3	71.7	270.2	.459E+06	32.43	9.29
1-41	5.48	92.3	99.5	88.1	139.2	71.3	269.6	.458E+06	28.84	8.21
1-43	5.48	92.4	99.5	88.3	138.4	71.2	269.3	.458E+06	26.38	7.50
1-44	5.50	92.4	99.2	87.8	136.8	71.0	270.9	.459E+06	22.40	6.31
1-45	5.51	92.4	99.2	88.2	136.2	71.3	271.2	.459E+06	20.58	5.79
1-47	5.47	92.4	99.4	87.7	138.2	71.7	269.5	.457E+06	22.34	6.37
1-49	5.52	92.3	99.5	88.1	138.9	71.4	272.0	.462E+06	18.68	5.22
50-1	5.49	92.3	99.1	88.1	135.2	71.1	270.4	.457E+06	2.88	.82

POOR ORIGINAL

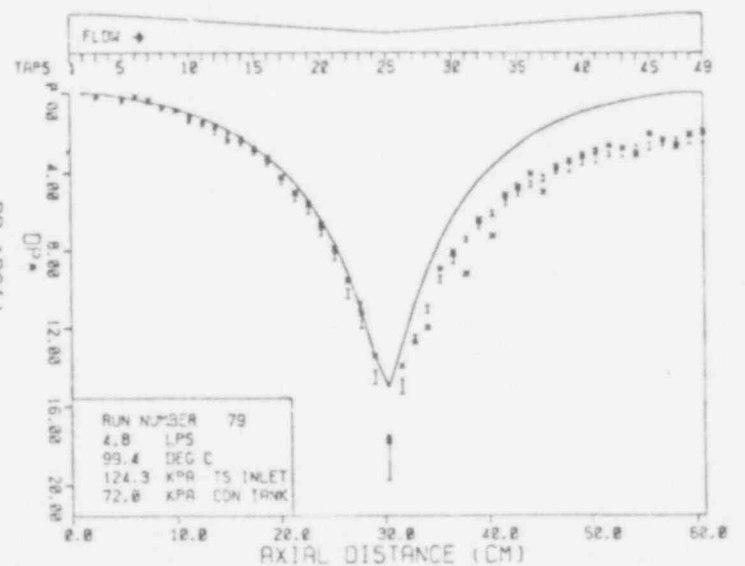
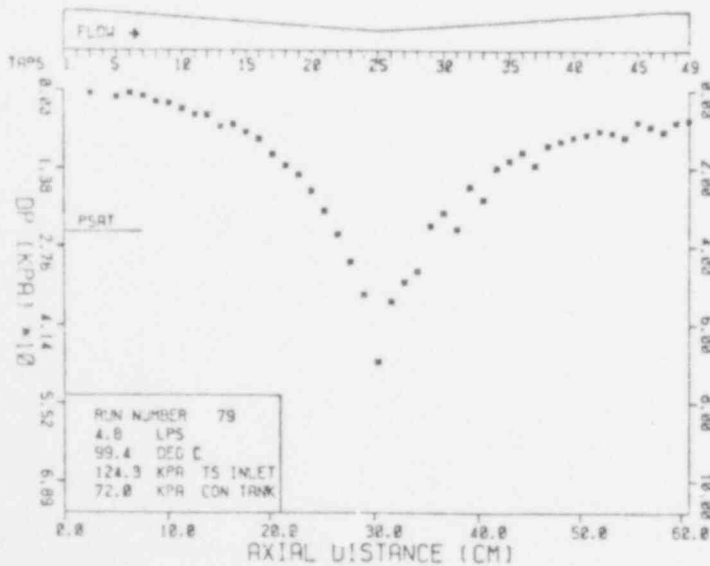


BNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2

RUN NUMBER 79

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-3	4.78	91.3	99.5	87.9	124.1	71.8	235.5	.400E+06	.55	.20
1-5	4.78	91.3	99.6	88.0	125.6	71.9	235.4	.401E+06	1.15	.43
1-6	4.79	91.3	99.3	87.8	123.9	71.3	235.9	.400E+06	.53	.20
1-7	4.81	91.3	99.1	87.5	122.9	71.5	237.1	.401E+06	1.04	.38
1-8	4.77	91.3	99.2	88.0	123.3	71.6	234.8	.398E+06	2.07	.78
1-9	4.77	91.3	99.8	88.2	125.8	71.9	234.8	.400E+06	2.32	.87
1-10	4.77	91.3	98.9	88.4	122.6	71.2	234.9	.397E+06	3.29	1.24
1-11	4.79	91.3	99.8	88.2	126.3	71.9	235.7	.401E+06	4.37	1.63
1-12	4.78	91.3	99.1	88.2	125.0	71.5	235.3	.398E+06	4.43	1.66
1-13	4.75	91.3	99.7	88.6	125.3	71.7	234.0	.398E+06	6.43	2.43
1-14	4.76	91.3	99.2	88.2	123.5	71.8	234.4	.397E+06	6.05	2.28
1-15	4.80	91.3	99.6	88.0	125.3	71.8	236.3	.402E+06	7.47	2.77
1-16	4.78	91.3	99.0	88.0	123.2	71.6	235.2	.398E+06	8.63	3.23
1-17	4.78	91.3	99.7	88.2	125.6	71.9	235.4	.400E+06	11.35	4.24
1-18	4.75	91.3	99.0	88.1	122.9	71.6	234.1	.396E+06	13.29	5.02
1-19	4.78	91.3	99.6	88.2	125.2	72.3	235.5	.400E+06	14.95	5.58
1-20	4.78	91.3	99.0	88.0	122.8	71.5	235.2	.397E+06	17.81	6.66
1-21	4.79	91.3	99.5	88.1	124.3	71.7	235.7	.400E+06	21.28	7.93
1-22	4.77	91.3	99.3	88.2	123.6	71.9	234.8	.398E+06	25.49	9.57
1-23	4.80	91.3	99.4	88.2	124.1	71.6	236.4	.401E+06	30.24	11.20
1-24	4.78	91.3	99.2	88.0	125.2	71.9	235.4	.399E+06	36.01	13.44
1-25	4.80	91.3	99.5	88.1	124.5	71.7	236.3	.401E+06	47.82	17.73
1-26	4.77	91.3	99.3	88.3	123.7	71.9	235.0	.398E+06	37.23	13.96
1-27	4.76	91.3	99.3	88.6	123.4	72.0	234.4	.397E+06	33.82	12.74
1-28	4.77	91.3	99.5	88.6	124.7	71.7	235.0	.399E+06	31.95	11.97
1-29	4.79	91.3	99.1	88.2	123.0	71.5	235.6	.398E+06	24.05	8.96
1-30	4.79	91.3	99.6	88.1	124.2	72.3	236.1	.401E+06	21.74	8.08
1-31	4.77	91.3	99.5	88.2	124.1	72.2	235.1	.399E+06	24.63	9.23
1-32	4.77	91.3	99.4	88.0	124.5	71.7	234.7	.398E+06	17.09	6.42
1-33	4.77	91.3	99.5	88.1	124.3	72.3	235.1	.399E+06	19.36	7.25
1-34	4.78	91.3	99.2	87.8	122.9	71.6	235.3	.398E+06	13.73	5.13
1-35	4.77	91.3	99.6	87.8	124.7	72.5	234.9	.399E+06	12.51	4.69
1-36	4.80	91.3	99.6	88.3	124.5	72.4	236.2	.401E+06	10.99	4.03
1-37	4.76	91.3	99.7	87.5	125.1	72.5	234.6	.399E+06	13.28	5.00
1-38	4.75	91.4	99.5	88.6	125.1	71.9	233.8	.397E+06	9.77	3.70
1-39	4.76	91.4	99.6	88.5	124.4	72.6	234.4	.398E+06	9.01	3.49
1-40	4.78	91.4	99.6	88.5	124.8	72.6	235.4	.400E+06	8.27	3.09
1-41	4.79	91.4	99.4	88.4	124.0	72.5	235.8	.400E+06	7.75	2.88
1-42	4.77	91.4	99.4	88.3	124.3	72.6	235.1	.399E+06	7.12	2.67
1-43	4.78	91.4	99.7	88.0	125.0	72.7	235.5	.400E+06	7.41	2.77
1-44	4.77	91.5	99.5	88.1	124.4	72.7	234.7	.398E+06	8.29	3.12
1-45	4.79	91.5	99.2	88.0	123.7	72.5	235.8	.399E+06	5.62	2.09
1-46	4.78	91.5	99.1	88.2	122.9	72.3	235.0	.398E+06	6.35	2.37
1-47	4.78	91.5	99.6	88.0	124.7	72.9	235.6	.400E+06	7.30	2.72
1-48	4.78	91.5	99.4	88.1	124.3	72.4	235.5	.400E+06	5.63	2.10
1-49	4.80	91.5	99.3	88.4	123.5	72.7	236.6	.401E+06	5.30	1.96
50-1	4.77	91.4	99.5	88.3	124.7	72.9	235.0	.399E+06	2.66	1.00

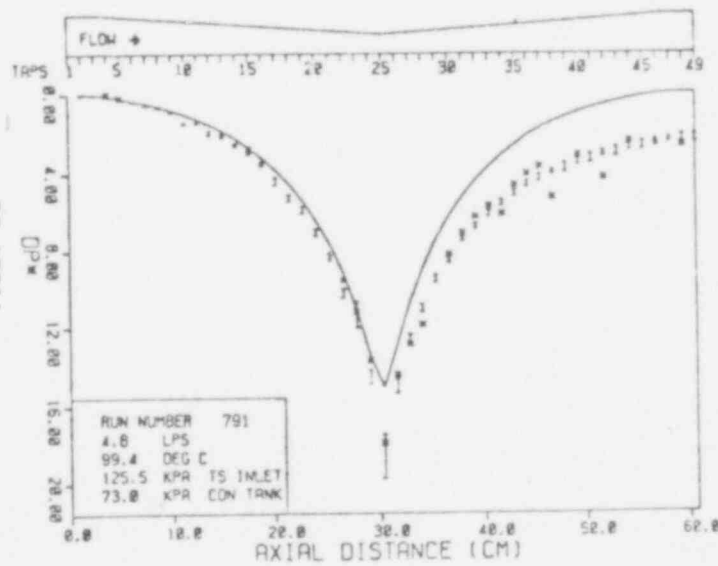
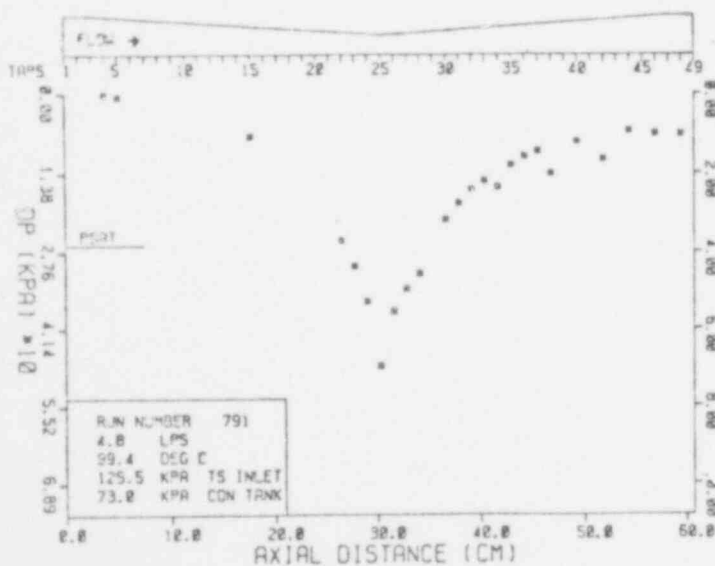
POOR ORIGINAL



BWL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM S/C	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
RUN NUMBER 791										
1-4	4.78	91.5	99.1	88.1	124.4	72.7	235.2	.398E+06	.00	.00
1-5	4.78	91.5	99.1	88.2	124.8	72.5	235.2	.398E+06	.52	.19
1-15	4.76	91.5	99.6	88.0	126.2	73.2	234.4	.399E+06	7.36	2.77
1-22	4.78	91.5	99.3	87.9	125.0	73.8	235.4	.399E+06	25.55	9.54
1-23	4.80	91.5	99.2	87.9	124.4	72.6	236.3	.400E+06	30.16	11.18
1-24	4.76	91.5	99.6	88.1	126.4	73.0	234.3	.398E+06	36.34	13.70
1-25	4.78	91.5	99.6	88.2	126.8	73.2	235.4	.400E+06	47.96	17.92
1-26	4.75	91.5	99.1	88.2	124.7	72.6	233.8	.395E+06	38.10	14.17
1-27	4.76	91.5	99.6	88.1	126.1	73.1	234.3	.398E+06	34.11	12.87
1-28	4.75	91.5	99.3	88.0	125.4	72.7	234.0	.396E+06	31.43	11.88
1-30	4.76	91.5	99.6	88.2	126.8	73.1	234.4	.398E+06	21.91	8.26
1-31	4.78	91.5	99.6	87.8	126.2	73.2	235.3	.400E+06	19.83	7.11
1-32	4.77	91.5	99.1	87.9	124.4	72.7	235.6	.397E+06	16.68	6.25
1-33	4.78	91.5	99.5	87.9	125.0	73.3	235.3	.399E+06	15.26	5.70
1-34	4.77	91.5	99.4	87.1	125.2	73.2	234.8	.398E+06	16.29	6.12
1-35	4.77	91.5	99.2	87.8	124.5	72.7	234.8	.398E+06	12.44	4.67
1-36	4.76	91.5	99.7	88.0	126.7	73.4	234.5	.399E+06	10.98	4.10
1-37	4.80	91.5	99.6	88.0	126.1	73.4	236.5	.402E+06	10.10	3.74
1-38	4.74	91.5	99.7	88.4	126.7	73.3	233.6	.397E+06	13.90	5.27
1-40	4.77	91.5	99.2	88.1	124.8	72.8	235.0	.398E+06	8.44	3.16
1-42	4.75	91.5	99.6	88.1	126.1	73.4	233.8	.397E+06	11.37	4.30
1-44	4.76	91.6	99.2	87.2	124.4	72.7	234.3	.397E+06	6.59	2.49
1-46	4.78	91.5	99.6	88.0	126.5	73.4	235.6	.400E+06	7.07	2.64
1-48	4.77	91.5	99.2	88.2	125.0	72.8	234.3	.397E+06	7.07	2.65
50-1	4.78	91.6	99.1	88.0	124.6	73.0	235.3	.398E+06	1.28	.48

POOR ORIGINAL

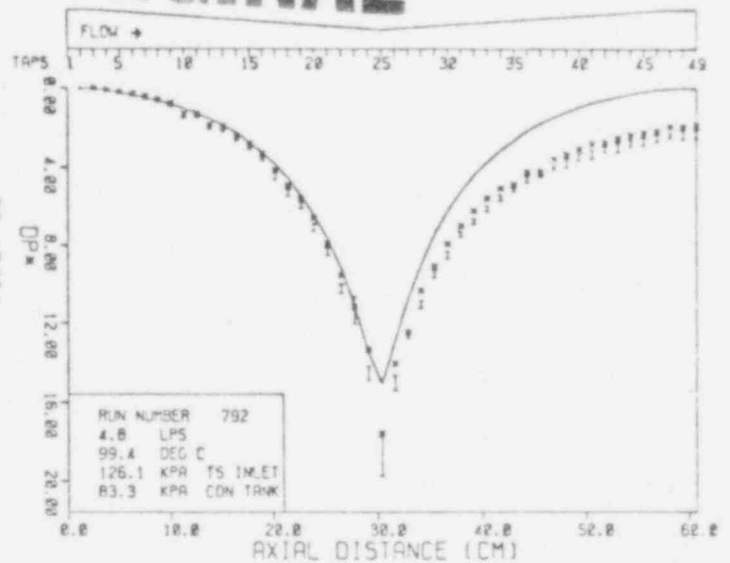
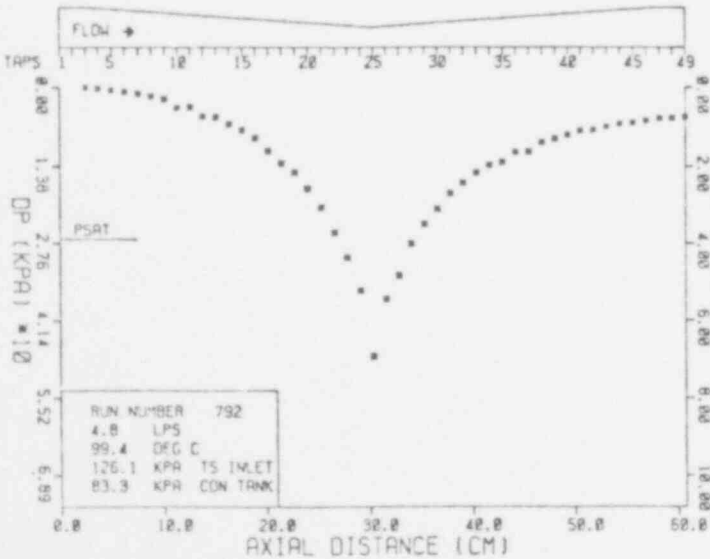


**BNL FLASHING FLOWS EXPERIMENT  
PRESSURE DROP DATA FROM  
TEST SECTION # 2**

RUN NUMBER 792

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-3	4.78	91.3	99.2	88.1	124.8	82.8	235.3	.398E+06	.00	.00
1-4	4.77	91.3	99.0	88.3	125.0	83.0	235.8	.397E+06	.20	.07
1-5	4.79	91.3	99.0	88.2	125.6	83.0	235.8	.399E+06	.50	.19
1-6	4.77	91.2	99.7	88.4	126.7	83.4	234.7	.399E+06	.75	.28
1-7	4.80	91.2	99.8	88.0	126.7	83.5	236.2	.402E+06	1.09	.41
1-8	4.81	91.3	98.9	88.0	125.2	82.8	236.8	.400E+06	1.58	.55
1-9	4.76	91.2	99.8	88.4	126.6	83.4	234.6	.399E+06	2.02	.76
1-10	4.79	91.3	99.2	88.0	124.7	82.8	235.8	.399E+06	3.51	1.31
1-11	4.75	91.3	99.7	88.3	128.2	83.6	234.1	.398E+06	3.37	1.27
1-12	4.76	91.3	99.1	88.3	124.4	82.7	234.4	.397E+06	4.90	1.86
1-13	4.78	91.2	99.6	88.2	126.9	83.6	235.3	.400E+06	5.15	1.93
1-14	4.79	91.4	99.2	88.3	124.9	82.8	235.8	.399E+06	6.43	2.39
1-15	4.77	91.2	99.3	88.4	125.9	83.4	234.9	.398E+06	7.42	2.78
1-16	4.78	91.2	99.2	88.4	124.7	82.8	235.3	.399E+06	8.84	3.30
1-17	4.79	91.3	99.7	88.2	125.8	83.7	236.0	.401E+06	11.12	4.14
1-18	4.80	91.3	98.9	88.2	125.0	82.8	236.4	.399E+06	13.22	4.90
1-19	4.75	91.3	99.8	88.4	127.1	83.5	234.1	.399E+06	14.80	5.59
1-20	4.79	91.2	99.0	88.3	126.0	83.0	235.7	.398E+06	17.69	6.59
1-21	4.76	91.3	99.8	88.5	126.8	83.5	234.6	.400E+06	21.06	7.92
1-22	4.78	91.3	99.1	88.3	125.7	83.1	235.4	.398E+06	25.57	9.55
1-23	4.79	91.3	99.6	87.9	125.9	83.2	236.1	.401E+06	30.08	11.17
1-24	4.80	91.3	99.0	88.1	125.6	83.1	236.5	.400E+06	36.01	13.32
1-25	4.81	91.3	99.8	87.9	127.2	83.6	237.0	.404E+06	47.72	17.59
1-26	4.77	91.3	99.0	88.2	125.6	83.1	235.0	.397E+06	37.50	14.05
1-27	4.78	91.3	99.8	88.0	126.5	83.6	235.4	.401E+06	33.36	12.47
1-28	4.78	91.3	99.1	87.9	125.0	82.8	235.1	.398E+06	27.62	10.33
1-29	4.76	91.3	99.4	88.2	127.3	83.5	234.2	.397E+06	24.11	9.10
1-30	4.81	91.3	99.8	88.2	127.0	83.8	236.6	.403E+06	21.46	7.93
1-31	4.77	91.3	99.7	88.8	126.7	83.2	234.8	.399E+06	18.63	7.00
1-32	4.80	91.4	99.1	87.9	125.1	83.2	236.5	.400E+06	16.79	6.21
1-33	4.79	91.3	99.4	88.3	125.9	83.5	235.6	.400E+06	14.91	5.56
1-34	4.78	91.3	99.2	87.7	125.2	83.0	235.5	.399E+06	13.59	5.07
1-35	4.78	91.4	99.6	88.1	125.9	83.7	235.2	.400E+06	13.06	4.89
1-36	4.78	91.4	99.4	88.2	125.9	83.1	235.3	.399E+06	11.29	4.22
1-37	4.77	91.3	99.8	87.9	128.9	83.6	234.7	.399E+06	11.24	4.23
1-38	4.77	91.4	99.0	88.1	125.3	82.9	234.8	.397E+06	9.57	3.59
1-39	4.77	91.4	99.0	88.0	125.6	83.0	235.0	.397E+06	8.94	3.35
1-40	4.80	91.3	99.7	88.1	126.9	83.5	236.1	.402E+06	8.30	3.08
1-41	4.78	91.3	99.8	88.0	127.1	83.6	235.6	.401E+06	7.58	2.83
1-42	4.80	91.4	99.6	88.0	126.2	83.3	236.3	.402E+06	7.37	2.73
1-43	4.79	91.3	99.2	87.8	126.3	83.3	236.0	.400E+06	6.85	2.55
1-44	4.78	91.3	99.3	87.5	125.6	83.3	235.3	.399E+06	6.35	2.37
1-45	4.80	91.3	99.7	87.9	126.8	83.3	236.3	.402E+06	6.14	2.28
1-46	4.76	91.3	99.7	88.2	126.7	83.4	234.4	.399E+06	5.76	2.17
1-47	4.80	91.4	99.7	88.1	127.0	83.6	236.4	.402E+06	5.36	1.99
1-48	4.79	91.3	99.6	88.1	126.1	83.6	235.7	.401E+06	5.32	1.98
1-49	4.78	91.4	99.3	88.4	125.9	83.4	235.5	.399E+06	5.11	1.91
50-1	4.78	91.4	99.6	88.3	126.1	83.6	235.4	.400E+06	2.63	.98

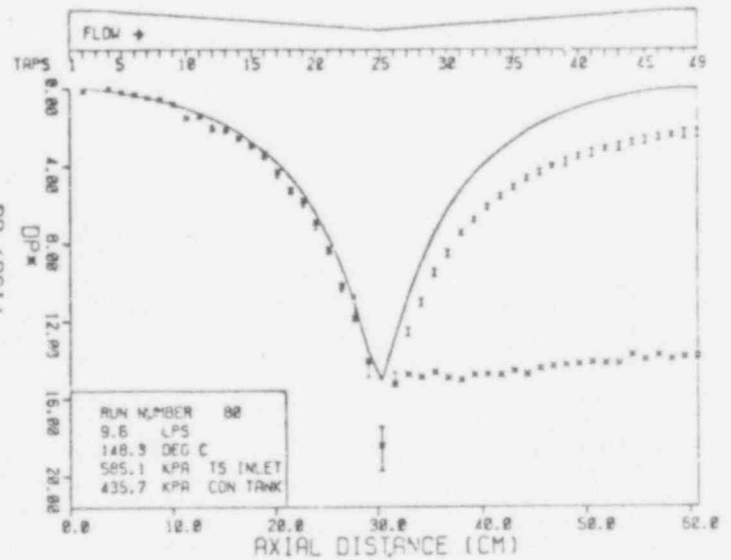
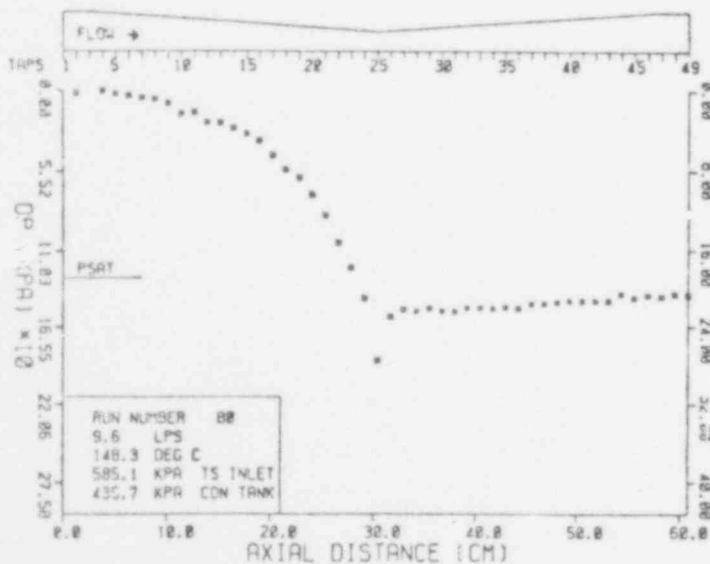
**POOR ORIGINAL**



# POOR ORIGINAL

## BNL FLASHING FLOWS EXPERIMENT PRESSURE DROP DATA FROM TEST SECTION # 2

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-2	9.61	204.0	148.8	144.4	591.5	442.0	473.1	.117E+07	1.25	.12
1-4	9.56	143.1	148.6	144.4	588.5	439.6	470.8	.117E+07	.00	.00
1-5	9.58	143.1	148.6	143.8	588.1	438.7	471.9	.117E+07	1.81	.16
1-6	9.58	143.1	148.5	143.9	586.5	438.3	471.8	.117E+07	3.38	.33
1-7	9.60	143.0	148.5	143.6	585.6	437.9	472.5	.117E+07	4.96	.48
1-8	9.59	143.0	148.4	143.7	587.6	436.5	472.3	.117E+07	5.74	.56
1-9	9.57	142.9	148.4	143.8	585.1	436.0	471.4	.116E+07	8.16	.79
1-10	9.61	142.8	148.3	143.5	583.1	435.1	473.1	.117E+07	15.76	1.52
1-11	9.58	142.9	148.3	143.1	586.6	435.0	471.9	.117E+07	14.78	1.43
1-12	9.57	142.9	148.3	143.5	584.6	434.9	471.4	.116E+07	21.68	2.11
1-13	9.58	142.8	148.3	143.7	585.3	434.7	471.9	.116E+07	22.40	2.17
1-14	9.56	142.9	148.3	143.8	584.9	435.1	471.0	.116E+07	26.05	2.54
1-15	9.59	142.9	148.3	143.8	585.2	435.2	472.2	.117E+07	29.79	2.89
1-16	9.55	142.9	148.3	143.7	583.1	435.2	470.3	.116E+07	34.45	3.35
1-17	9.58	142.9	148.3	143.6	583.7	435.4	471.6	.116E+07	44.35	4.31
1-18	9.57	142.9	148.3	143.4	584.6	435.4	471.1	.116E+07	53.95	5.25
1-19	9.60	142.9	148.3	143.5	585.4	435.1	472.7	.117E+07	59.64	5.76
1-20	9.59	142.9	148.3	143.6	586.7	435.2	472.4	.117E+07	70.99	6.87
1-21	9.58	142.9	148.3	143.5	583.6	435.5	471.6	.116E+07	85.23	8.27
1-22	9.56	142.9	148.3	143.5	583.9	435.5	470.9	.116E+07	104.54	10.18
1-23	9.58	142.9	148.3	143.5	585.8	435.4	472.0	.117E+07	122.36	11.86
1-24	9.58	142.9	148.3	143.1	583.8	435.4	471.6	.116E+07	144.64	14.05
1-25	9.57	142.9	148.3	143.4	583.1	435.3	471.2	.116E+07	189.46	18.42
1-26	9.60	142.9	148.3	143.7	582.7	435.4	472.9	.117E+07	158.04	15.26
1-27	9.60	142.9	148.3	143.5	581.6	435.7	472.8	.117E+07	152.88	14.77
1-28	9.60	142.9	148.3	143.5	584.0	435.5	472.5	.117E+07	153.58	14.88
1-29	9.62	143.0	148.3	143.2	582.8	435.7	473.9	.117E+07	152.20	14.64
1-30	9.59	142.9	148.4	143.5	584.4	435.9	472.0	.117E+07	153.92	14.92
1-31	9.56	142.9	148.4	143.4	584.4	435.9	470.6	.116E+07	154.28	15.04
1-32	9.56	142.9	148.3	143.4	586.0	435.8	470.8	.116E+07	151.65	14.77
1-33	9.57	142.9	148.3	143.5	587.4	435.8	471.5	.116E+07	151.69	14.74
1-34	9.57	142.9	148.3	143.3	584.9	435.5	471.0	.116E+07	151.93	14.79
1-35	9.60	142.9	148.3	143.3	585.1	435.5	472.8	.117E+07	150.94	14.58
1-36	9.57	142.8	148.3	143.4	585.8	435.3	471.2	.116E+07	151.73	14.76
1-37	9.57	142.9	148.3	143.4	585.3	435.3	471.4	.116E+07	148.54	14.43
1-38	9.59	142.8	148.3	143.1	584.9	434.7	472.4	.117E+07	148.24	14.34
1-39	9.59	142.9	148.3	143.2	585.3	434.8	472.1	.117E+07	147.18	14.26
1-40	9.57	142.8	148.3	143.4	585.0	434.8	471.4	.116E+07	146.38	14.23
1-41	9.60	142.8	148.3	143.3	586.5	434.7	472.8	.117E+07	146.40	14.14
1-42	9.58	142.8	148.3	143.2	582.9	434.4	471.8	.116E+07	146.31	14.19
1-43	9.59	142.8	148.3	143.5	585.2	435.1	472.0	.117E+07	146.30	14.18
1-44	9.58	142.8	148.3	143.3	584.8	435.3	471.9	.117E+07	141.82	13.75
1-45	9.58	142.8	148.3	143.0	585.9	435.1	471.6	.116E+07	144.12	13.99
1-46	9.60	142.9	148.3	143.5	585.0	435.1	472.6	.117E+07	142.49	13.77
1-47	9.56	142.8	148.3	143.4	586.1	435.4	470.6	.116E+07	143.47	13.99
1-48	9.55	142.8	148.3	143.4	584.8	435.1	470.2	.116E+07	141.86	13.86
1-49	9.58	142.8	148.3	143.2	582.4	435.2	471.7	.116E+07	142.68	13.85
50-1	9.58	142.8	148.3	143.7	585.9	435.3	471.6	.116E+07	13.22	1.28





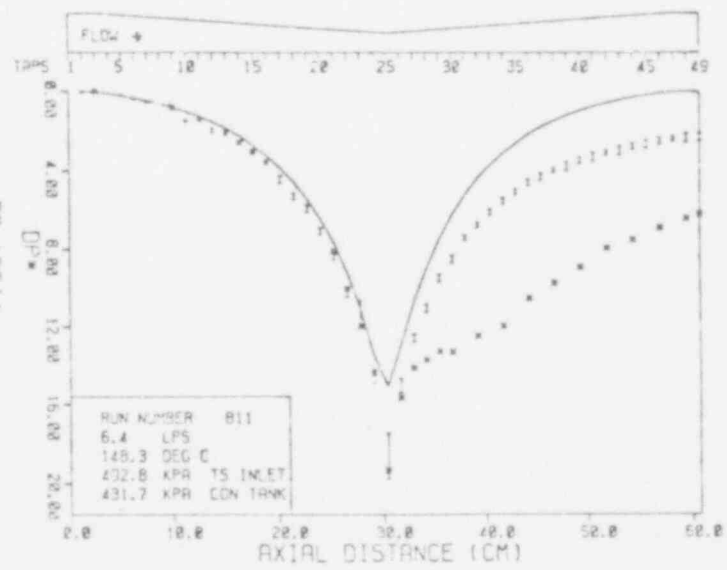
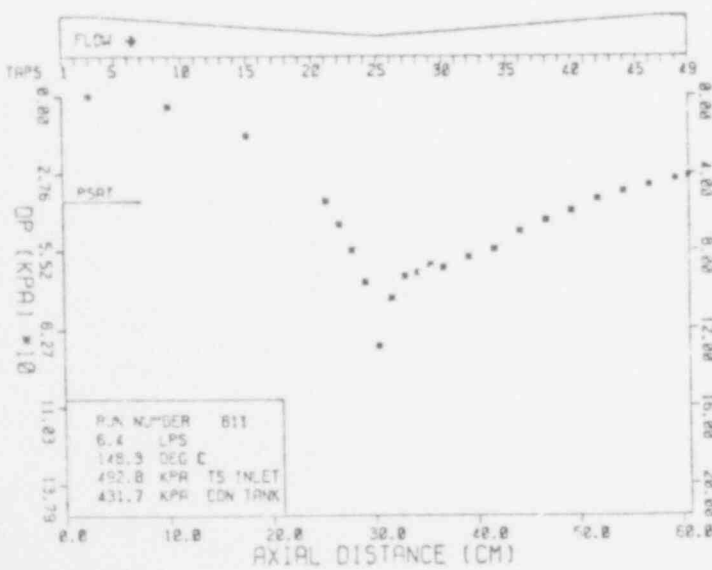




BNL FLASHING FLOWS EXPERIMENT  
 PRESSURE DROP DATA FROM  
 TEST SECTION # 2

TAPS	LOOP FLOW LTR/SEC	TEMPERATURES (DEG C)			PRESSURE (KPA)		VELOCITY CM SEC	REYNOLDS NUMBER	DIFFERENTIAL PRESSURE	
		FLOW METER	TS INLET	COND TANK	TS INLET	COND TANK			MEASURED	DIMENSIONLESS
1-3	6.39	139.3	148.3	144.7	493.0	431.0	314.8	.777E+06	.00	.00
1-9	6.38	139.3	148.3	145.0	493.8	430.9	314.4	.776E+06	3.66	.80
1-15	6.37	139.3	148.3	144.9	492.6	430.8	313.8	.775E+06	13.95	3.06
1-21	6.41	139.3	148.3	144.8	492.5	431.0	315.6	.779E+06	37.36	8.10
1-22	6.37	139.3	148.3	144.5	493.8	431.1	313.9	.775E+06	45.81	10.04
1-23	6.40	139.3	148.3	144.9	492.5	430.9	315.3	.779E+06	55.08	11.96
1-24	6.40	139.3	148.4	144.8	493.8	431.7	315.1	.778E+06	66.14	14.39
1-25	6.39	139.3	148.3	144.6	492.5	431.3	314.6	.777E+06	88.50	19.31
1-26	6.40	139.3	148.4	144.6	493.0	431.7	315.3	.779E+06	72.02	15.64
1-27	6.37	139.4	148.3	144.7	492.6	431.5	313.7	.775E+06	64.28	14.11
1-28	6.40	139.4	148.3	144.7	492.4	431.7	315.1	.778E+06	62.93	13.69
1-29	6.36	139.4	148.3	144.7	492.0	431.7	313.4	.774E+06	60.32	13.36
1-30	6.41	139.4	148.4	144.6	492.5	431.9	315.4	.779E+06	61.24	12.79
1-32	6.41	139.4	148.4	144.7	492.6	431.8	315.4	.779E+06	57.49	12.48
1-34	6.39	139.4	148.4	144.6	492.6	432.0	314.5	.779E+06	54.81	11.97
1-36	6.39	139.5	148.3	144.6	492.4	431.7	314.8	.778E+06	48.44	10.35
1-38	6.37	139.4	148.3	144.5	492.7	431.9	313.4	.774E+06	44.36	9.25
1-40	6.38	139.4	148.4	144.6	492.7	432.1	314.4	.777E+06	40.96	8.35
1-42	6.41	139.4	148.4	144.8	492.8	432.0	315.6	.780E+06	36.67	7.95
1-44	6.35	139.5	148.4	144.4	492.3	432.1	312.8	.773E+06	34.08	7.52
1-46	6.40	139.4	148.4	144.1	493.1	432.1	315.1	.778E+06	31.73	6.90
1-48	6.39	139.5	148.4	144.5	492.4	432.2	314.9	.778E+06	29.47	6.42
1-49	6.39	139.5	148.4	144.5	492.7	432.3	314.5	.777E+06	28.42	6.21
50-1	6.39	139.5	148.4	144.6	493.0	432.7	314.6	.777E+06	5.24	1.14

POOR ORIGINAL



575 213













## VOID FRACTION DISTRIBUTION DATA

## FLASHING EXPERIMENTS

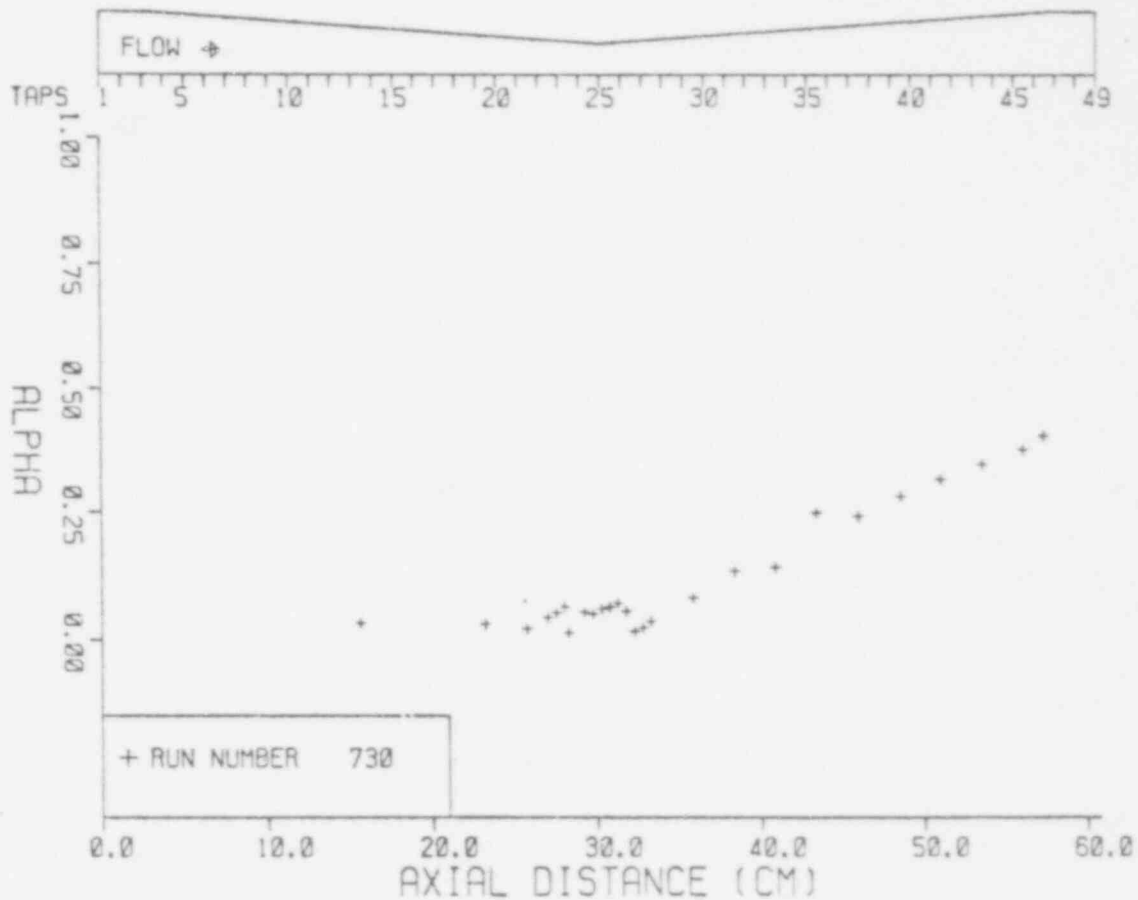
RUN	$p_{in}$ (kPa)	$T_{in}$ ( $^{\circ}$ C)	$G$ (Mg/m <sup>2</sup> s)	$p_{ct}$ (kPa)	$T_{ct}$ ( $^{\circ}$ C)
730	285	99.4	4.91	54	88.0
740	285	99.4	4.91	54	88.0
762	394	99.3	6.05	61	88.3
770	157	99.3	3.05	67	88.5
771	157	99.3	3.05	67	88.5
780	138	99.3	2.61	71	88.1
781	138	99.3	2.61	71	88.1
792	125	99.4	2.26	76	88.1
793	125	99.4	2.26	76	88.1
801	582	148.3	4.34	434	143.5
802	582	148.3	4.34	434	143.5
812	493	148.3	2.91	431	144.4
813	493	148.3	2.91	431	144.4
821	376	142.3	2.34	175	111.3
822	376	142.3	2.34	175	111.3
831	350	140.0	2.30	147	107.5
832	350	140.0	2.30	147	107.5

POOR ORIGINAL

BNL FLASHING FLOWS EXPERIMENT  
 GAMMA DENSITOMETER DATA  
 TEST SECTION # 2

RUN NUMBER 730

LOCATION IN CM FROM TAP 49	AVERAGE NUMBER OF COUNTS IN 54 SEC	AVERAGE ALPHA	STD DEV
3.31	1265.	.40	.04
4.58	1237.	.38	.03
7.11	1242.	.35	.04
9.65	1207.	.37	.03
12.10	1206.	.28	.04
14.73	1209.	.24	.05
17.28	1243.	.25	.04
19.82	1232.	.14	.08
22.36	1236.	.13	.06
24.88	1220.	.08	.06
27.45	1257.	.04	.04
29.94	1321.	.02	.06
32.44	1385.	.02	.05
34.92	1378.	.06	.09
37.48	1363.	.07	.09
39.98	1298.	.07	.08
42.48	1222.	.06	.07
44.91	1295.	.05	.06
47.32	1335.	.05	.07
49.77	1310.	.01	.08
52.17	1323.	.07	.06
54.54	1321.	.05	.06
56.85	1304.	.04	.05
59.19	1227.	.02	.05
61.52	1234.	.03	.06
63.82	1111.	.03	.05



-188-

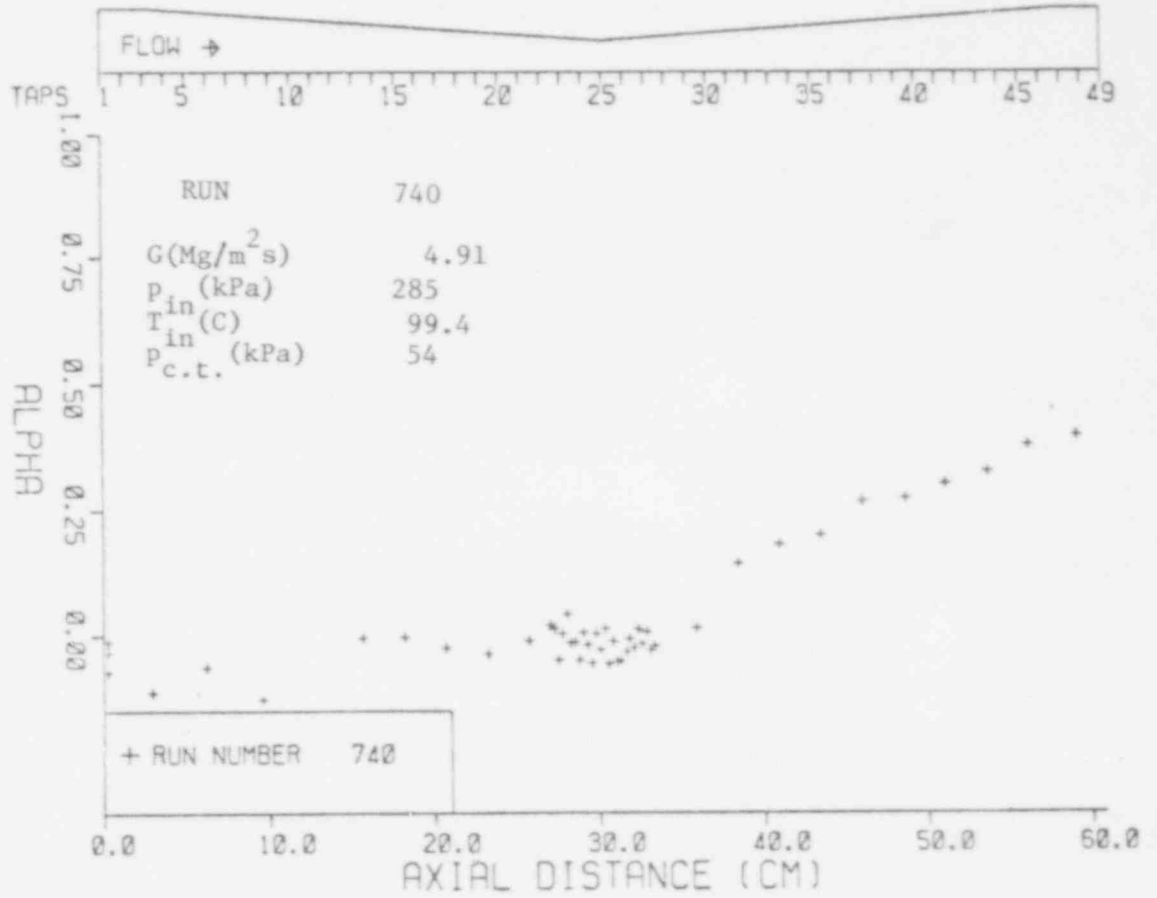
575 220

POOR ORIGINAL

BNL FLASHING FLOWS EXPERIMENT  
 GAMMA DENSITOMETER DATA  
 TEST SECTION # 2

RUN NUMBER 740

LOCATION IN CM FROM TAP #9	AVERAGE NUMBER OF COUNTS IN 54 SEC	AVERAGE ALPHA	STD DEV
3.31	1249.	.40	.03
4.58	1230.	.38	.04
7.11	1213.	.33	.04
9.65	1187.	.30	.04
12.10	1187.	.27	.02
14.73	1214.	.27	.05
17.28	1198.	.20	.04
19.82	1244.	.18	.05
22.36	1230.	.14	.06
24.88	1166.	.01	.06
27.45	1211.	-.02	.06
29.70	1260.	-.03	.07
32.94	1207.	-.01	.06
38.19	1331.	-.02	.08
38.44	1367.	.01	.04
38.71	1340.	.03	.09
39.92	1327.	-.01	.06
41.20	1293.	-.03	.06
42.44	1280.	-.05	.06
43.73	1269.	-.05	.07
44.98	1240.	-.01	.06
46.24	1198.	-.06	.05
47.48	1186.	-.01	.06
48.74	1204.	-.03	.06
50.00	1257.	.00	.08
51.25	1247.	-.05	.04
52.51	1382.	-.02	.08
53.76	1314.	.00	.05
55.01	1288.	-.05	.06
56.26	1265.	-.01	.06
57.52	1281.	-.01	.05
58.77	1233.	-.04	.10
60.02	1254.	-.00	.08
61.27	1253.	-.05	.05
62.53	1281.	.01	.07
63.78	1277.	.02	.07
65.05	1197.	-.01	.07
66.30	1183.	-.04	.04
67.55	1140.	-.02	.07
68.81	1097.	-.00	.06
70.06	1076.	-.00	.04
71.31	989.	-.13	.06
72.56	940.	-.06	.04
73.81	911.	-.11	.05
75.06	896.	-.07	.05
76.31	909.	-.03	.05
77.56	902.	-.01	.05

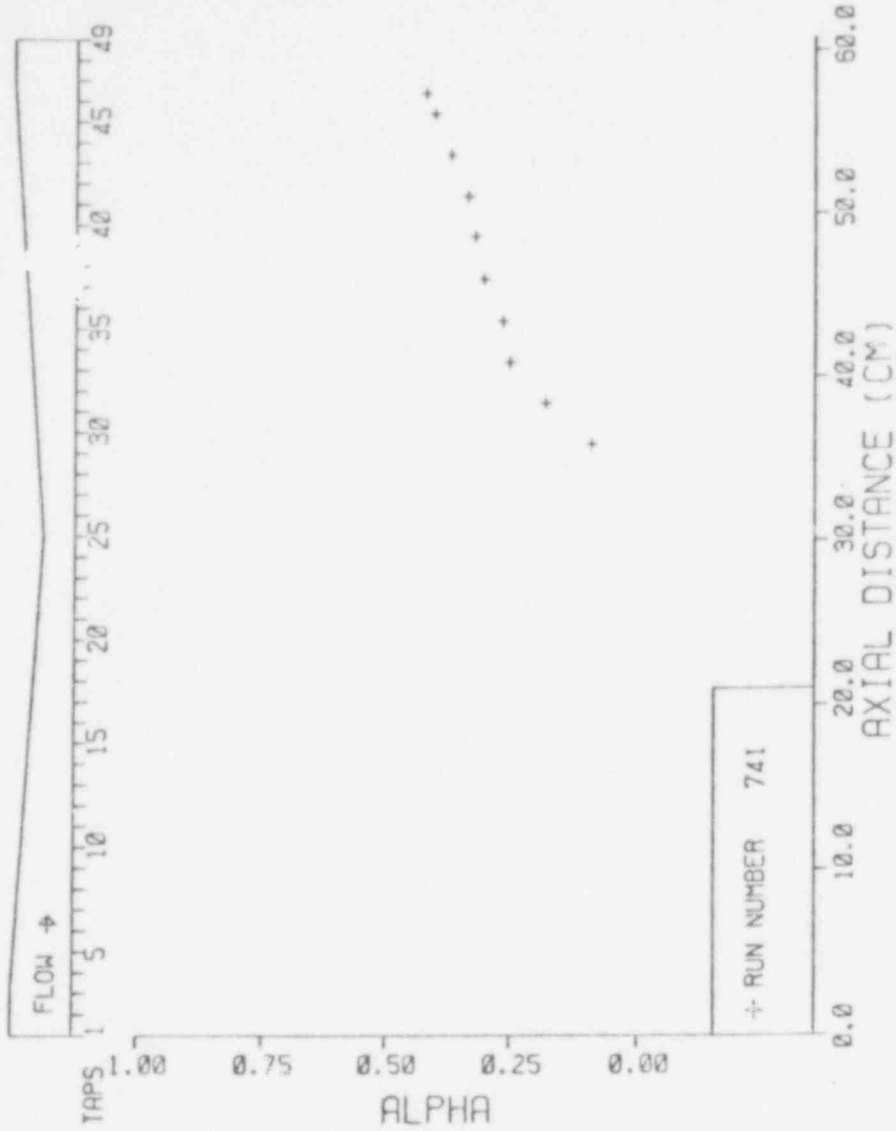


POOR ORIGINAL

-189-  
575  
221

BML FLASHING FLOWS EXPERIMENT  
GARYA BUBBLIOMETER DATA  
TEST SECTION # 2

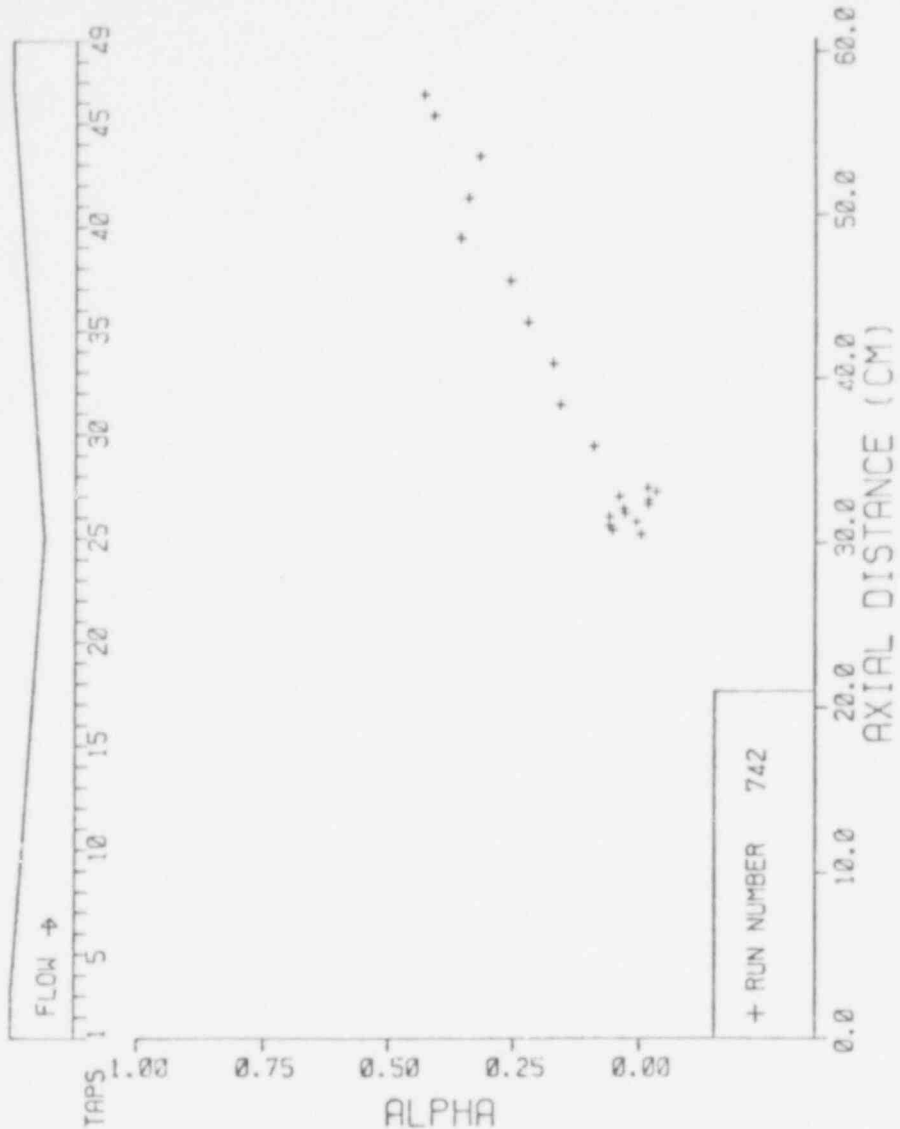
LOCATION IN CM FROM TAP #3	RUN NUMBER	AVERAGE OF COUNTS IN 54 SEC	AVERAGE ALPHA	STD DEV
3.31	741	1772	.42	.05
4.54		1523	.41	.04
7.16		1530	.37	.04
8.61		1534	.34	.04
12.10		1545	.32	.06
14.72		1545	.27	.03
17.74		1793	.24	.03
19.87		1555	.18	.05
23.36		1213	.09	.07
24.88				



POOR ORIGINAL

BML FLASHING PLOWS EXPERIMENT  
GAMMA DENSITOMETER DATA  
TEST SECTION # 2

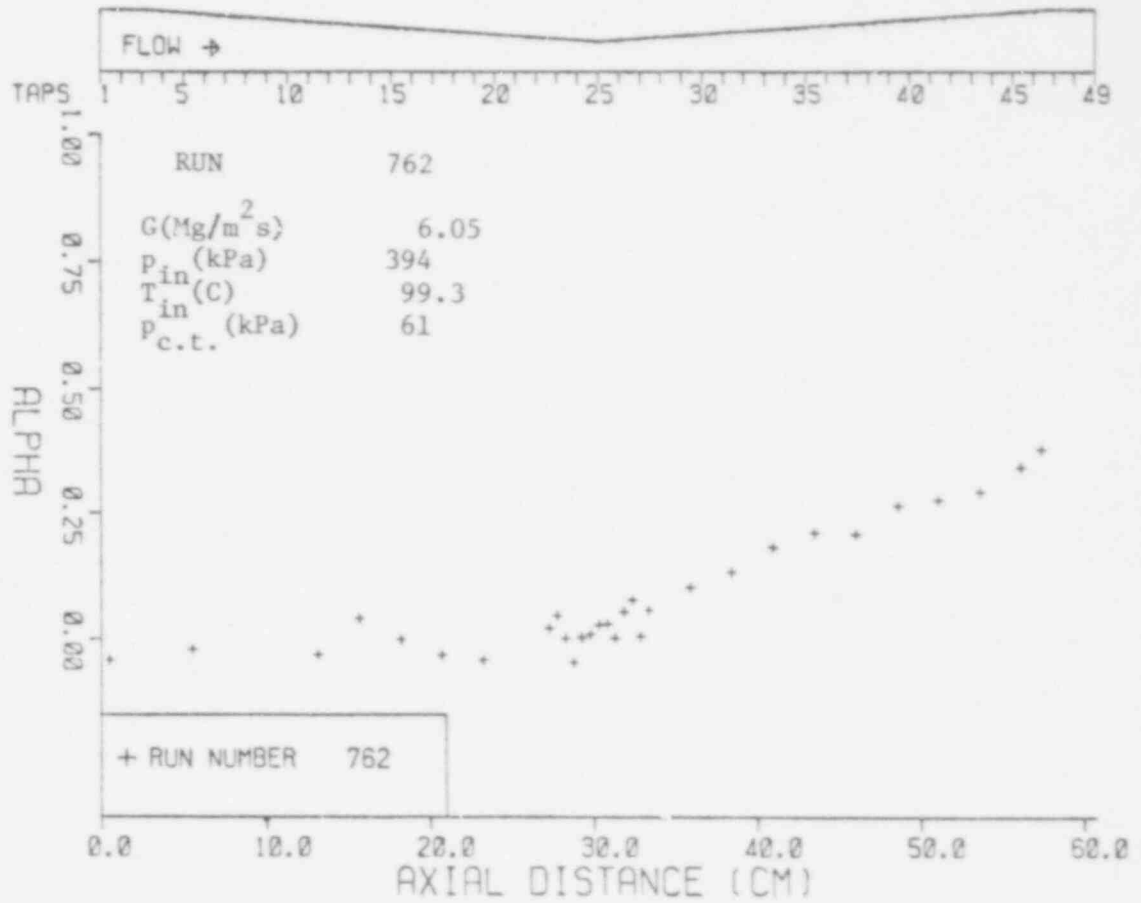
LOCATION IN CN FROM TAP #1	RUN NUMBER	742	AVERAGE COUNTS IN 54 SEC	AVERAGE ALPHA	STD DEV
3.31	1286			-.43	.03
4.58	1265			-.41	.05
7.11	1212			-.22	.04
9.65	1222			-.24	.04
12.10	1253			-.26	.05
14.73	1213			-.26	.05
17.26	1219			-.22	.08
19.80	1242			-.17	.07
22.36	1248			-.16	.05
24.88	1218			-.09	.08
27.45	1221			-.02	.07
30.00	1264			-.03	.07
32.94	1354			.04	.06
35.48	1327			.02	.08
38.44	1228			.02	.05
41.71	1355			.03	.07
44.92	1343			.03	.04
48.20	1318			.06	.04
51.48	1337			.01	.06
54.73	1285			.06	.06
58.04	1230			.05	.07
61.24				-.00	.07



**POOR ORIGINAL**

BNL FLASHING FLOWS EXPERIMENT  
 GAMMA DENSITOMETER DATA  
 TEST SECTION # 2

LOCATION IN CX FROM TAP 49	AVERAGE NUMBER OF COUNTS IN 54 SEC	AVERAGE ALPHA	STD DEV
3.31	1222.	.38	.02
4.58	1188.	.34	.03
7.11	1178.	.29	.04
9.65	1155.	.28	.05
12.10	1173.	.26	.05
14.73	1164.	.20	.05
17.28	1196.	.21	.05
19.82	1236.	.18	.05
22.36	1216.	.13	.05
24.88	1210.	.10	.06
27.45	1249.	.06	.04
27.94	1289.	.01	.06
29.44	1327.	.08	.06
28.92	1354.	.05	.05
29.44	1301.	.00	.07
29.98	1257.	.03	.09
30.48	1186.	.03	.09
31.00	1253.	.01	.05
31.51	1285.	.00	.06
32.01	1241.	.05	.05
32.52	1242.	.00	.08
33.02	1270.	.05	.06
33.53	1279.	.02	.03
37.59	1174.	.03	.03
40.15	1130.	.03	.09
42.67	1153.	.00	.05
45.22	1098.	.03	.04
47.75	1041.	.03	.05
55.39	923.	.03	.05
60.45	877.	.03	.05



-192-

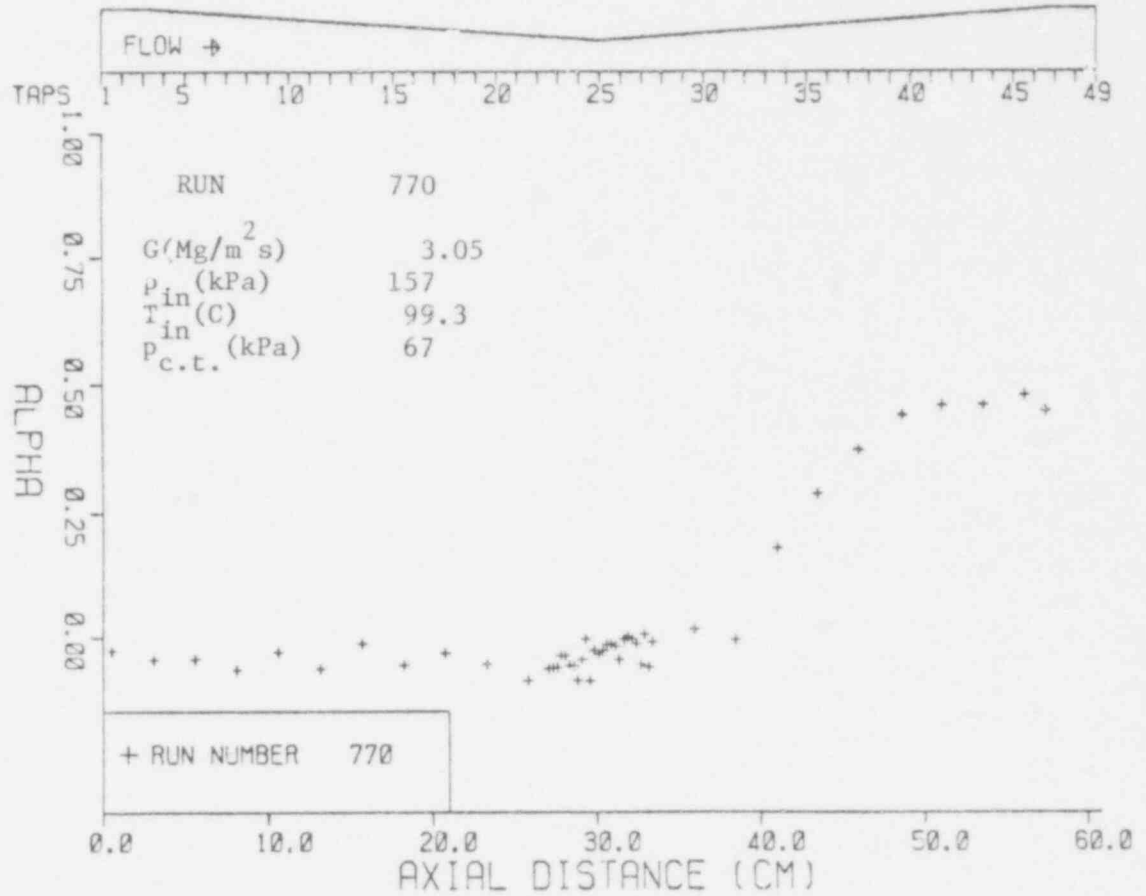
575 224

POOR ORIGINAL

BNI, FLASHING FLOWS EXPERIMENT  
 GAMMA DENSITOMETER DATA  
 TEST SECTION # 2

RUN NUMBER 770

LOCATION IN CM FROM TAP 49	AVERAGE NUMBER OF COUNTS IN 54 SEC	AVERAGE ALPHA	STD DEV
3.31	1287.	.45	.04
4.58	1315.	.48	.02
7.11	1319.	.46	.04
9.65	1306.	.46	.03
12.10	1212.	.44	.05
14.73	1284.	.37	.03
17.28	1251.	.29	.05
19.82	1237.	.18	.06
22.36	1136.	-.01	.09
24.88	1160.	-.01	.07
27.45	1211.	-.01	.06
27.70	1237.	-.06	.08
27.94	1289.	-.01	.04
28.19	1303.	-.06	.08
28.44	1345.	-.01	.05
28.71	1344.	-.00	.02
28.92	1324.	-.00	.05
29.20	1301.	-.01	.06
29.48	1276.	-.05	.06
29.73	1280.	-.02	.05
29.98	1232.	-.02	.05
30.24	1211.	-.02	.09
30.45	1161.	-.03	.10
30.74	1194.	-.04	.09
31.08	1236.	-.03	.11
31.25	1224.	-.09	.08
31.51	1282.	-.00	.08
31.76	1272.	-.05	.06
31.91	1260.	-.09	.08
32.26	1264.	-.06	.06
32.52	1252.	-.06	.08
32.77	1249.	-.04	.07
33.02	1225.	-.04	.03
33.27	1239.	-.06	.07
33.53	1235.	-.06	.08
33.78	1226.	-.06	.06
35.05	1151.	-.09	.07
37.59	1168.	-.05	.06
40.15	1129.	-.03	.04
42.67	1061.	-.06	.04
45.22	1065.	-.01	.03
47.75	1022.	-.06	.08
50.29	955.	-.03	.05
52.83	935.	-.07	.06
55.39	908.	-.04	.04
57.91	896.	-.05	.05
60.45	887.	-.03	.05



-193-

575 225

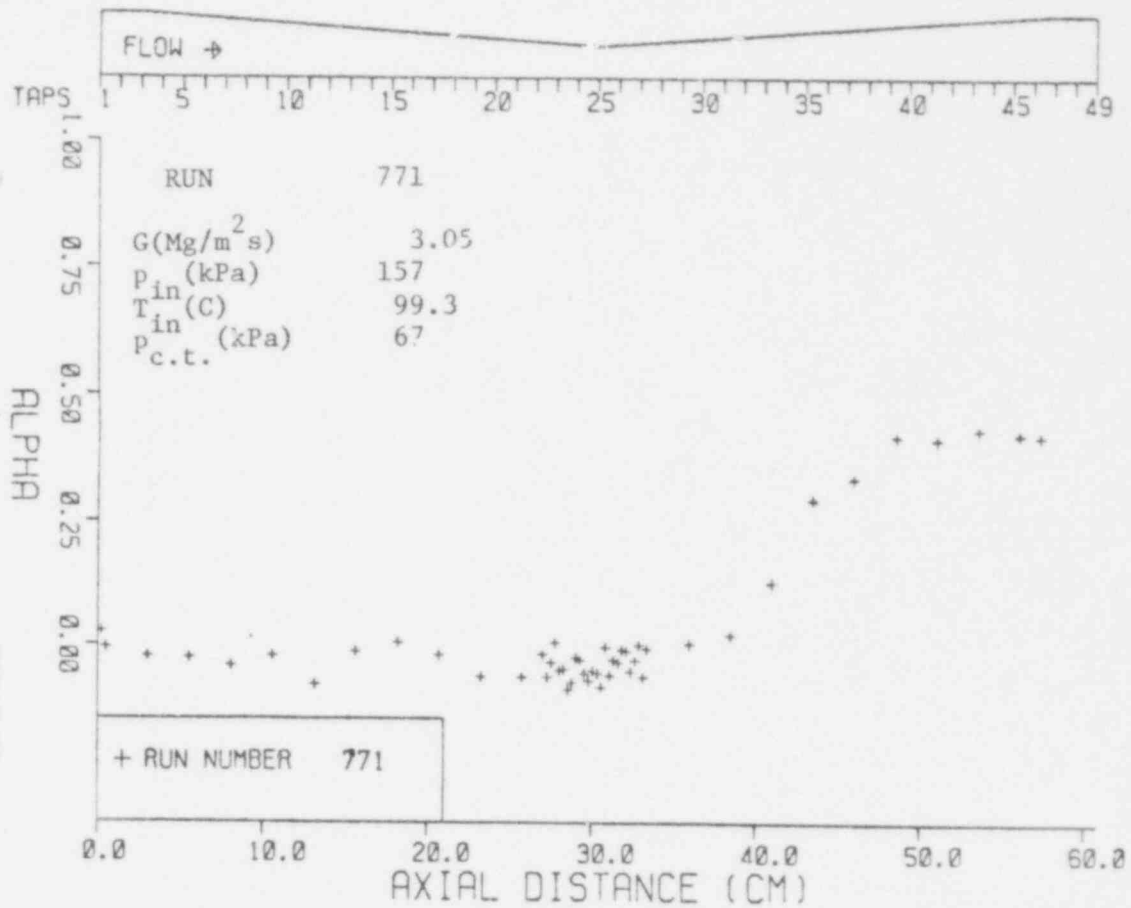
POOR ORIGINAL

BNL FLASHING FLOWS EXPERIMENT  
GAMMA DENSITOMETER DATA  
TEST SECTION # 2

RUN NUMBER 771

LOCATION IN CM FROM TAP 49	AVERAGE NUMBER OF COUNTS IN 54 SEC	AVERAGE ALPHA	STD DEV
3.31	1254.	.42	.04
4.58	1256.	.42	.05
7.11	1288.	.43	.05
9.65	1261.	.41	.04
12.10	1288.	.42	.06
14.73	1249.	.33	.05
17.28	1250.	.29	.05
19.82	1194.	.12	.05
22.36	1145.	.02	.06
24.88	1147.	.00	.06
27.45	1206.	-.01	.06
27.70	1228.	-.07	.07
27.94	1250.	.00	.04
28.19	1310.	-.03	.10
28.44	1317.	-.05	.08
28.71	1333.	-.01	.07
28.92	1313.	-.01	.05
29.20	1278.	-.03	.06
29.48	1277.	-.03	.06
29.73	1250.	-.06	.06
29.98	1232.	-.00	.06
30.24	1172.	-.09	.06
30.48	1142.	-.06	.06
30.74	1180.	-.05	.05
31.00	1207.	-.07	.09
31.25	1233.	-.06	.08
31.51	1262.	-.03	.08
31.76	1275.	-.03	.09
32.01	1259.	-.08	.05
32.26	1241.	-.09	.07
32.52	1249.	-.05	.09
32.77	1236.	-.05	.10
33.02	1242.	-.01	.08
33.27	1246.	-.04	.06
33.53	1227.	-.07	.07
33.78	1243.	-.02	.04
35.05	1156.	-.07	.07
37.59	1156.	-.07	.06
40.15	1129.	-.02	.02
42.67	1091.	.01	.06
45.22	1140.	-.01	.08
47.75	1115.	-.08	.06
50.29	954.	-.02	.05
52.83	914.	-.04	.06
55.39	914.	-.02	.05
57.91	906.	-.02	.06
60.45	897.	-.00	.06

-194-



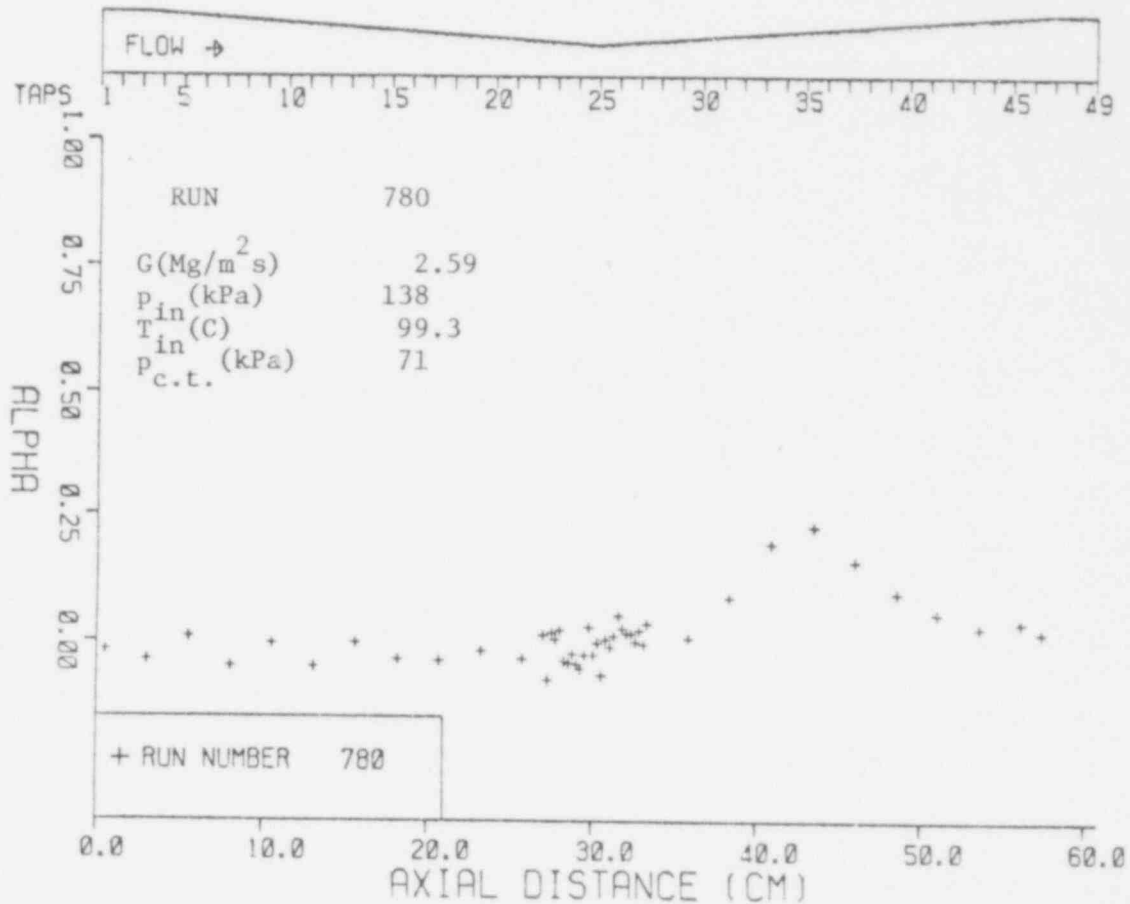
575 226



BNL FLASHING FLOWS EXPERIMENT  
 GAMMA DENSITOMETER DATA  
 TEST SECTION # 2

RUN NUMBER 780

LOCATION IN CM FROM TAP 49	AVERAGE NUMBER OF COUNTS IN 54 SEC	AVERAGE ALPHA	STD DEV
3.31	931.	.02	.04
4.58	942.	.04	.05
7.11	981.	.03	.06
9.65	933.	.06	.05
12.10	1052.	.10	.05
14.73	1127.	.16	.04
17.28	1203.	.23	.07
19.82	1238.	.19	.04
22.36	1184.	.09	.08
24.88	1149.	.01	.06
27.45	1230.	.04	.06
27.70	1259.	.01	.06
27.94	1292.	.02	.07
28.19	1327.	.00	.07
28.44	1355.	.02	.06
28.71	1349.	.02	.06
28.92	1331.	.03	.06
29.20	1327.	.05	.05
29.48	1300.	.01	.08
29.73	1277.	.01	.05
29.98	1235.	.00	.04
30.24	1180.	.07	.07
30.48	1166.	.00	.05
30.74	1191.	.03	.04
31.00	1256.	.03	.06
31.25	1247.	.03	.07
31.51	1250.	.05	.06
31.76	1266.	.04	.07
32.01	1287.	.02	.07
32.26	1266.	.04	.05
32.52	1255.	.04	.05
32.77	1253.	.02	.07
33.02	1241.	.00	.05
33.27	1273.	.02	.04
33.53	1222.	.08	.06
33.78	1260.	.01	.07
35.05	1172.	.03	.06
37.59	1180.	.02	.07
40.15	1119.	.04	.05
42.67	1066.	.04	.06
45.22	1066.	.00	.05
47.75	1023.	.05	.04
50.29	965.	.00	.06
52.83	939.	.05	.03
55.39	937.	.01	.08
57.91	896.	.04	.03
60.45	888.	.02	.05

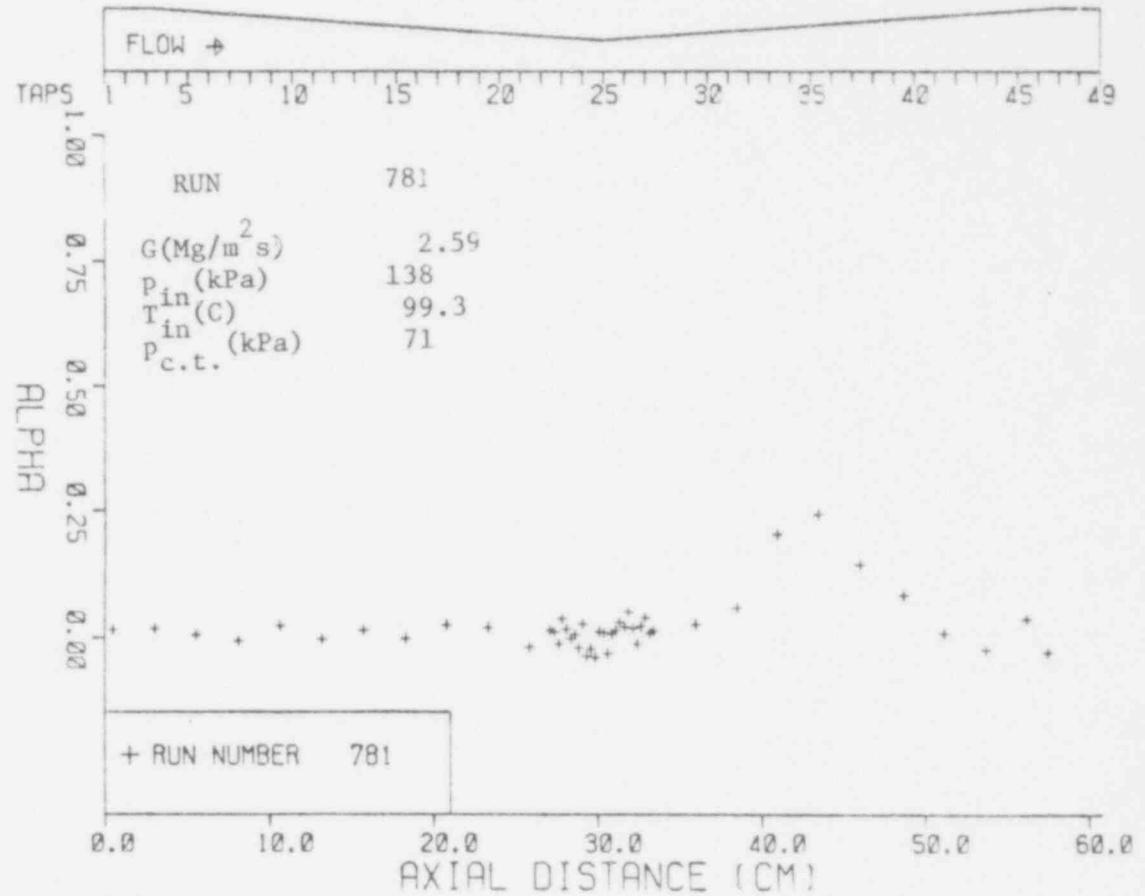


-195-

575 227

BNL FLASHING FLOWS EXPERIMENT  
 GAMMA DENSITOMETER DATA  
 TEST SECTION # 2

LOCATION IN CM FROM TAP 49	AVERAGE NUMBER OF COUNTS IN 54 SEC	AVERAGE ALPHA	STD DEV
3.31	894.	-.03	.05
4.58	934.	-.03	.03
7.11	941.	-.02	.04
9.65	956.	-.01	.04
12.10	1036.	-.08	.06
14.73	1111.	-.14	.06
17.28	1205.	-.24	.06
19.82	1238.	-.29	.05
22.36	1159.	-.06	.05
24.88	1153.	-.02	.04
27.45	1210.	-.01	.07
27.70	1260.	-.01	.10
27.94	1294.	-.04	.06
28.19	1332.	-.02	.07
28.44	1332.	-.01	.10
28.71	1342.	-.02	.08
28.92	1337.	-.05	.05
29.20	1361.	-.02	.06
29.48	1303.	-.03	.09
29.73	1283.	-.01	.09
29.98	1231.	-.01	.06
30.24	1190.	-.03	.07
30.48	1165.	-.01	.07
30.74	1203.	-.01	.07
31.00	1216.	-.04	.08
31.25	1242.	-.02	.02
31.51	1252.	-.04	.09
31.76	1293.	-.02	.07
32.01	1281.	-.02	.05
32.26	1284.	-.01	.05
32.52	1266.	-.00	.07
32.77	1262.	-.01	.06
33.02	1251.	-.04	.07
33.27	1251.	-.01	.07
33.53	1259.	-.01	.05
33.78	1253.	-.01	.06
35.05	1173.	-.02	.07
37.59	1195.	-.02	.07
40.15	1149.	-.02	.07
42.67	1081.	-.00	.10
45.22	1070.	-.01	.04
47.75	1047.	-.00	.07
50.29	977.	-.02	.04
52.83	961.	-.01	.04
55.39	929.	-.00	.05
57.91	928.	-.02	.05
60.45	905.	-.02	.02



-196-

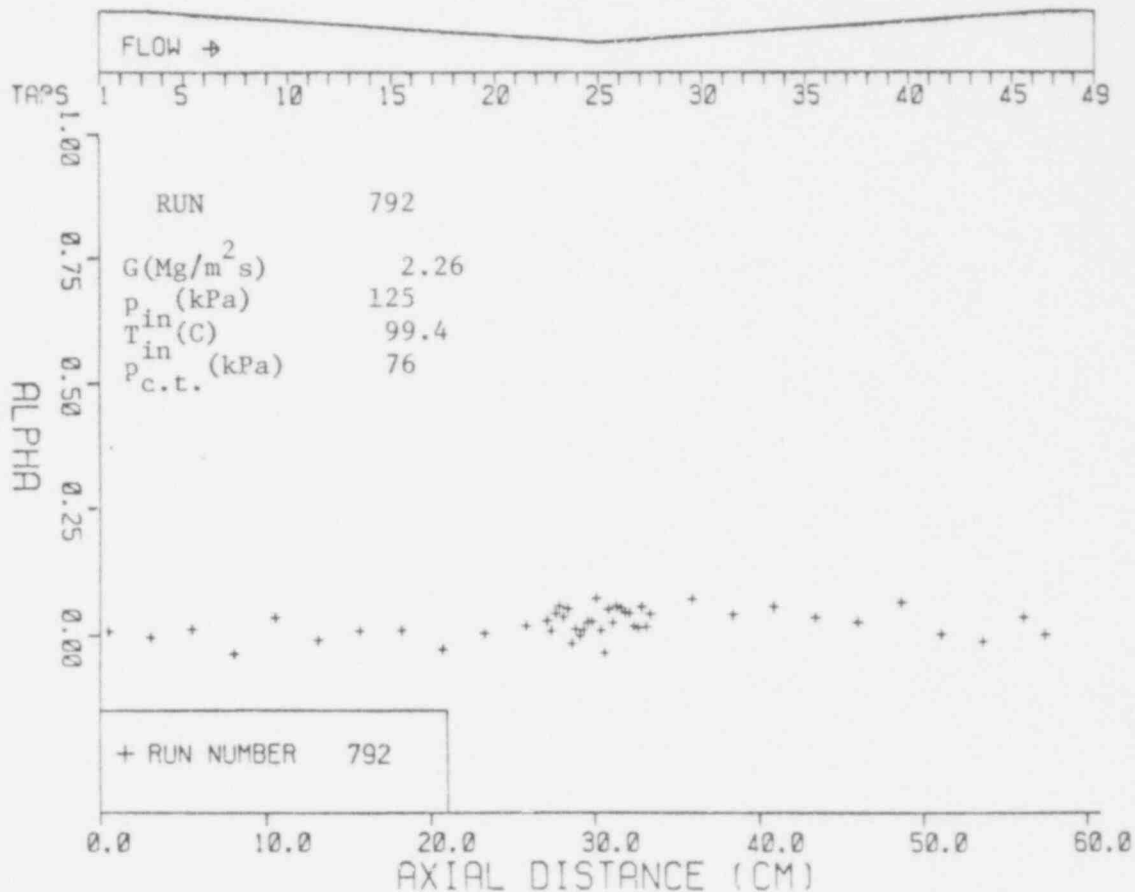
575 228

POOR ORIGINAL

BNL FLASHING FLOWS EXPERIMENT  
GAMMA DENSITOMETER DATA  
TEST SECTION # 2

RUN NUMBER 792

LOCATION IN CM FROM TAP 49	AVERAGE NUMBER OF COUNTS IN 54 SEC	AVERAGE ALPHA	STD DEV
3.31	915.	.00	.05
4.58	935.	.04	.05
7.11	944.	.01	.03
9.65	953.	.00	.05
12.10	1025.	.07	.05
14.7	1037.	.13	.06
17.24	1072.	.03	.06
19.82	1146.	.06	.07
22.36	1150.	.04	.07
24.88	1180.	.07	.05
27.45	1227.	.04	.06
27.70	1264.	.12	.06
27.94	1305.	.06	.08
28.19	1329.	.02	.06
28.44	1349.	.02	.06
28.71	1358.	.04	.05
28.92	1335.	.05	.05
29.20	1321.	.05	.06
29.48	1318.	.06	.08
29.73	1289.	.13	.06
29.98	1256.	.05	.08
30.24	1189.	.03	.07
30.48	1166.	.01	.09
30.74	1233.	.07	.09
31.00	1250.	.03	.09
31.25	1267.	.03	.05
31.51	1277.	.01	.07
31.76	1280.	.00	.07
32.01	1299.	.01	.08
32.26	1273.	.02	.08
32.52	1296.	.05	.06
32.77	1273.	.04	.08
33.02	1263.	.06	.07
33.27	1281.	.04	.07
33.53	1259.	.01	.08
33.78	1262.	.03	.08
35.05	1193.	.02	.07
37.59	1187.	.00	.05
40.15	1120.	.03	.07
42.67	1087.	.01	.07
45.22	1067.	.01	.05
47.75	1043.	.01	.06
50.29	985.	.04	.05
52.83	942.	.04	.03
55.39	934.	.01	.05
57.91	913.	.00	.03
60.45	900.	.01	.04



POOR ORIGINAL

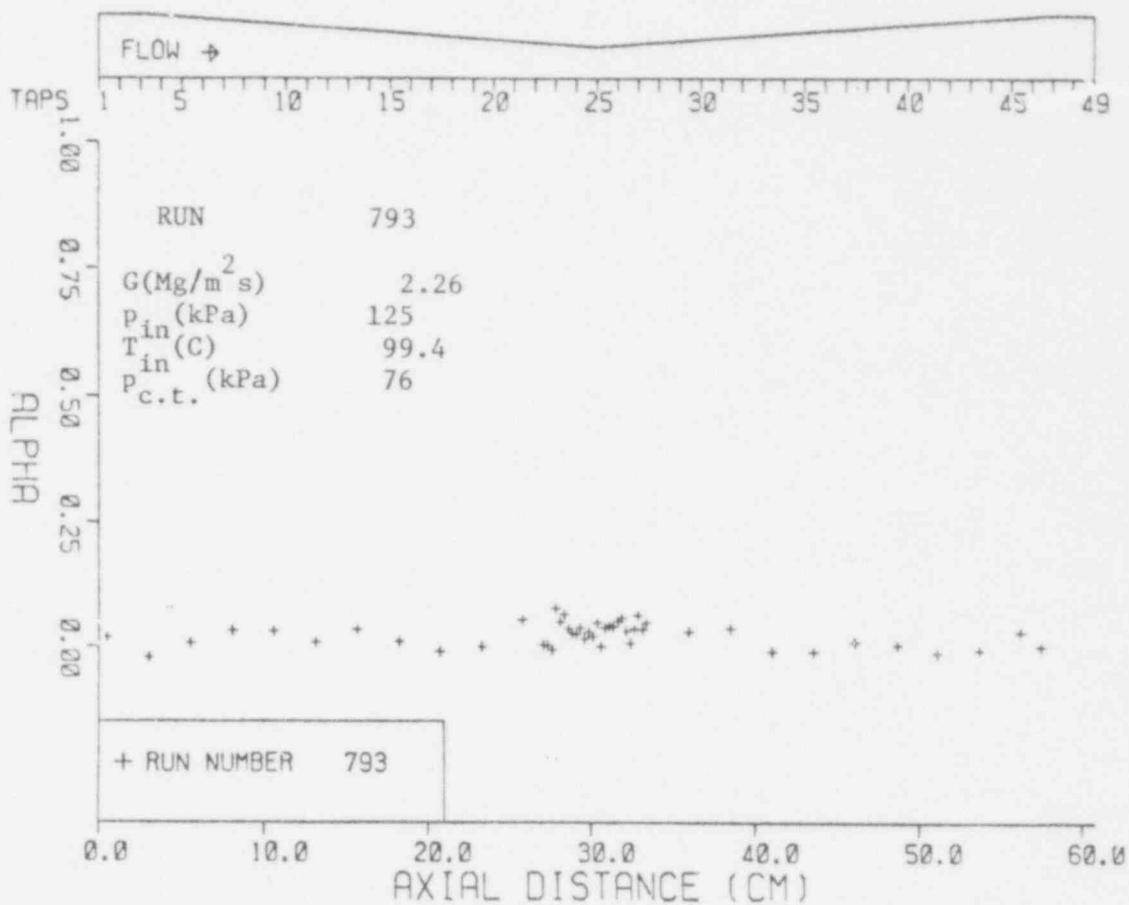
-197-

575 229

BNL FLASHING FLOWS EXPERIMENT  
 GAMMA DENSITOMETER DATA  
 TEST SECTION # 2

RUN NUMBER 793

LOCATION IN CM FROM TAP 49	AVERAGE NUMBER OF COUNTS IN 54 SEC	AVERAGE ALPHA	STD DEV
3.31	914.	.00	.04
4.58	930.	.03	.06
7.11	952.	-.01	.05
9.65	942.	-.01	.07
12.10	985.	.00	.06
14.73	1026.	.01	.03
17.28	1045.	-.01	.04
19.82	1106.	-.01	.04
22.36	1147.	.04	.06
24.88	1156.	.03	.09
27.45	1231.	.05	.06
27.70	1272.	.03	.07
27.94	1308.	.06	.04
28.19	1339.	.03	.05
28.44	1342.	.00	.06
28.71	1350.	.03	.07
28.92	1342.	.06	.07
29.20	1319.	.05	.03
29.48	1309.	.04	.11
29.73	1298.	.04	.06
29.98	1247.	.04	.06
30.24	1295.	.00	.07
30.48	1183.	.05	.05
30.74	1207.	.02	.07
31.00	1249.	.03	.08
31.25	1261.	.01	.07
31.51	1289.	.04	.05
31.76	1297.	.02	.06
32.01	1292.	.03	.06
32.26	1299.	.03	.04
32.52	1301.	.06	.05
32.77	1279.	.05	.06
33.02	1273.	.09	.08
33.27	1254.	-.01	.09
33.53	1255.	.00	.07
33.78	1248.	.00	.04
35.02	1212.	.05	.08
37.59	1184.	-.00	.10
40.15	1129.	-.01	.08
42.67	1087.	.01	.06
45.22	1083.	.03	.04
47.75	1053.	.01	.04
50.29	982.	.03	.06
52.83	986.	.03	.05
55.39	930.	-.01	.06
57.91	911.	-.02	.05
60.45	907.	-.02	.05



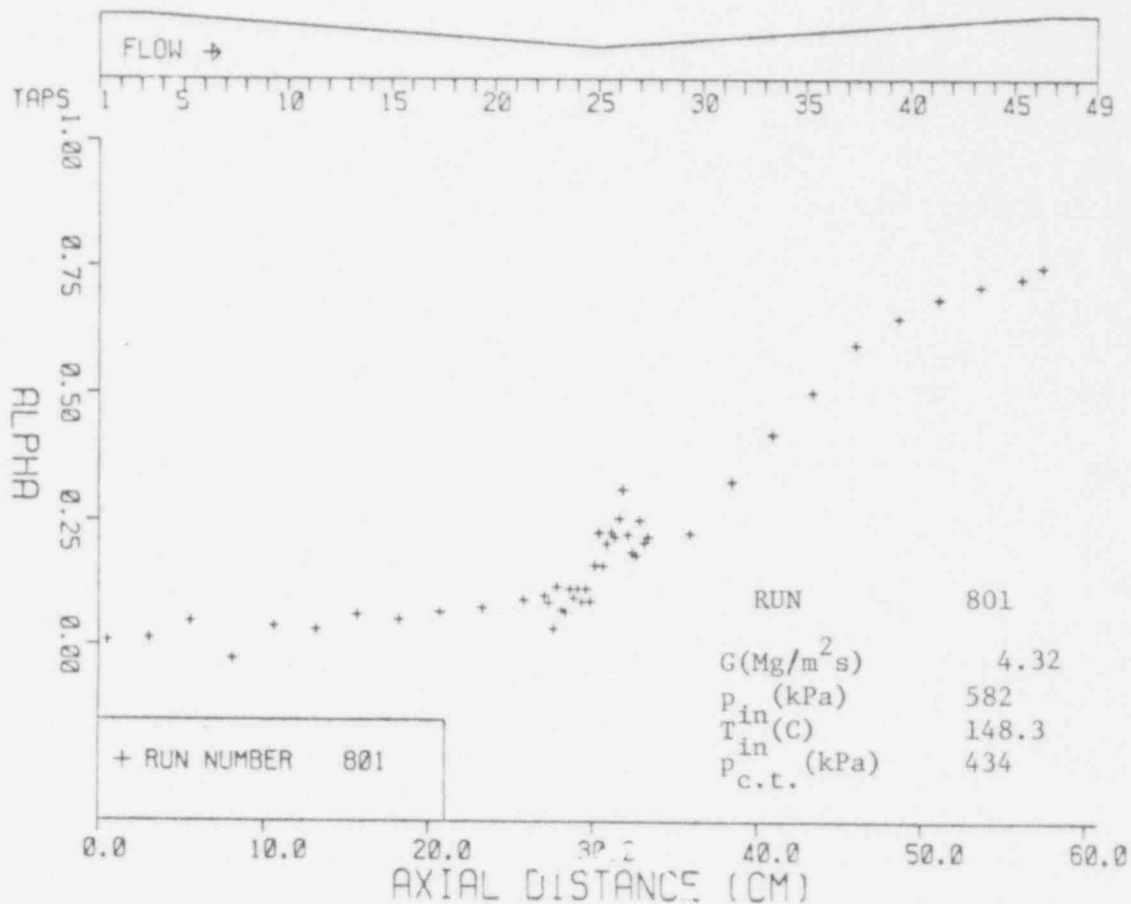
-198-

575 230

POOR ORIGINAL

DNT FLASHING FLOWS EXPERIMENT  
 GAMMA DENSITOMETER DATA  
 TEST SECTION # 2

LOCATION IN CM FROM TAP # 49	AVERAGE NUMBER OF COUNTS IN 54 SEC	RUN NUMBER 801	AVERAGE ALPHA	STD DEV
3.31	1597.		.75	.04
4.58	1575.		.73	.05
7.11	1553.		.71	.06
9.65	1512.		.69	.05
12.10	1487.		.65	.04
14.73	1455.		.60	.04
17.29	1407.		.50	.05
19.82	1398.		.42	.04
22.36	1339.		.33	.06
24.89	1287.		.23	.08
27.45	1345.		.22	.07
29.76	1381.		.21	.07
32.94	1435.		.25	.06
38.19	1438.		.18	.05
38.44	1460.		.19	.06
38.71	1479.		.22	.11
38.92	1502.		.31	.07
39.20	1454.		.25	.11
39.48	1421.		.22	.04
39.73	1412.		.23	.07
39.98	1355.		.28	.08
40.24	1297.		.16	.09
40.49	69772.		.23	.18
40.74	1289.		.16	.08
41.00	1367.		.09	.08
41.25	1324.		.12	.09
41.51	1331.		.09	.07
41.76	1349.		.11	.08
42.01	1372.		.10	.07
42.26	1354.		.11	.09
42.52	1317.		.07	.06
42.77	1305.		.07	.06
43.02	1309.		.12	.07
43.27	1290.		.03	.07
43.53	1314.		.10	.05
43.78	1314.		.09	.08
44.05	1247.		.09	.07
44.31	1242.		.08	.06
44.57	1190.		.07	.05
44.83	1130.		.05	.05
45.09	1118.		.06	.05
45.35	1089.		.03	.05
45.61	1007.		.04	.05
45.87	970.		.03	.05
46.13	979.		.04	.05
46.39	948.		.01	.07
46.65	924.		.01	.04



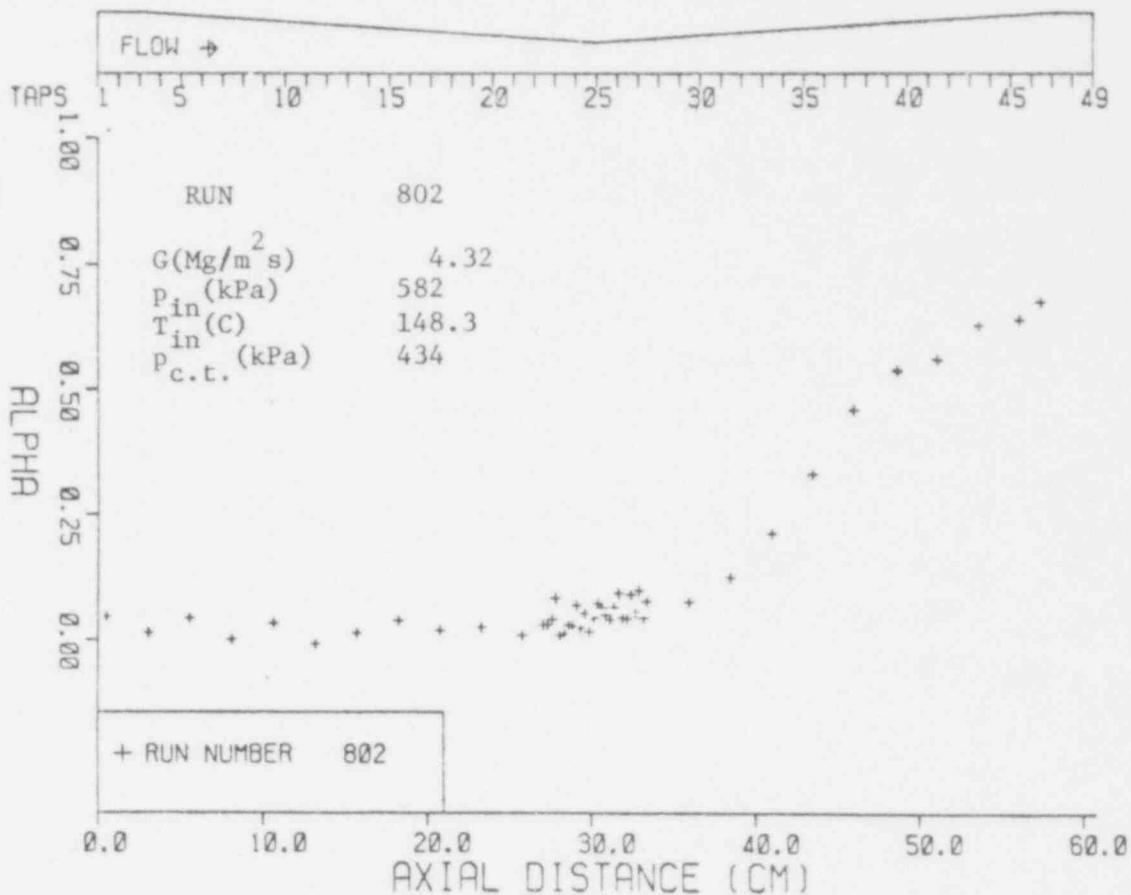
-199-

575 231

POOR ORIGINAL

BNL FLASHING FLOWS EXPERIMENT  
GAMMA DENSITOMETER DATA  
TEST SECTION # 2

LOCATION IN CM FROM TAP 49	AVERAGE NUMBER OF COUNTS IN 54 SEC	AVERAGE ALPHA	STD DEV
3.31	1506.	.68	.03
4.58	1467.	.64	.03
7.11	1460.	.63	.03
9.65	1384.	.56	.04
12.10	1382.	.54	.04
14.73	1341.	.46	.05
17.28	1275.	.33	.07
19.82	1252.	.21	.06
22.36	1208.	.12	.06
24.88	1193.	.08	.07
27.45	1256.	.08	.05
27.70	1287.	.04	.06
27.94	1337.	.10	.04
28.19	1359.	.06	.05
28.44	1398.	.09	.04
28.71	1367.	.14	.09
28.92	1343.	.05	.05
29.20	1352.	.09	.04
29.48	1330.	.07	.09
29.73	1305.	.04	.07
29.98	1263.	.05	.06
30.24	1243.	.07	.05
30.48	1200.	.07	.05
30.74	1226.	.04	.03
31.00	1250.	.02	.09
31.25	1287.	.05	.06
31.51	1290.	.02	.06
31.76	1320.	.07	.06
32.01	1314.	.03	.06
32.26	1303.	.03	.06
32.52	1281.	.01	.05
32.77	1266.	.01	.07
33.02	1284.	.08	.07
33.27	1287.	.04	.07
33.53	1278.	.03	.05
33.78	1271.	.03	.09
35.05	1197.	.01	.09
37.59	1208.	.03	.08
40.15	1157.	.02	.07
42.67	1117.	.04	.08
45.22	1084.	.01	.03
47.75	1058.	.01	.06
50.29	999.	.03	.05
52.83	983.	.00	.06
55.39	971.	.04	.06
57.91	943.	.01	.04
60.45	945.	.05	.05



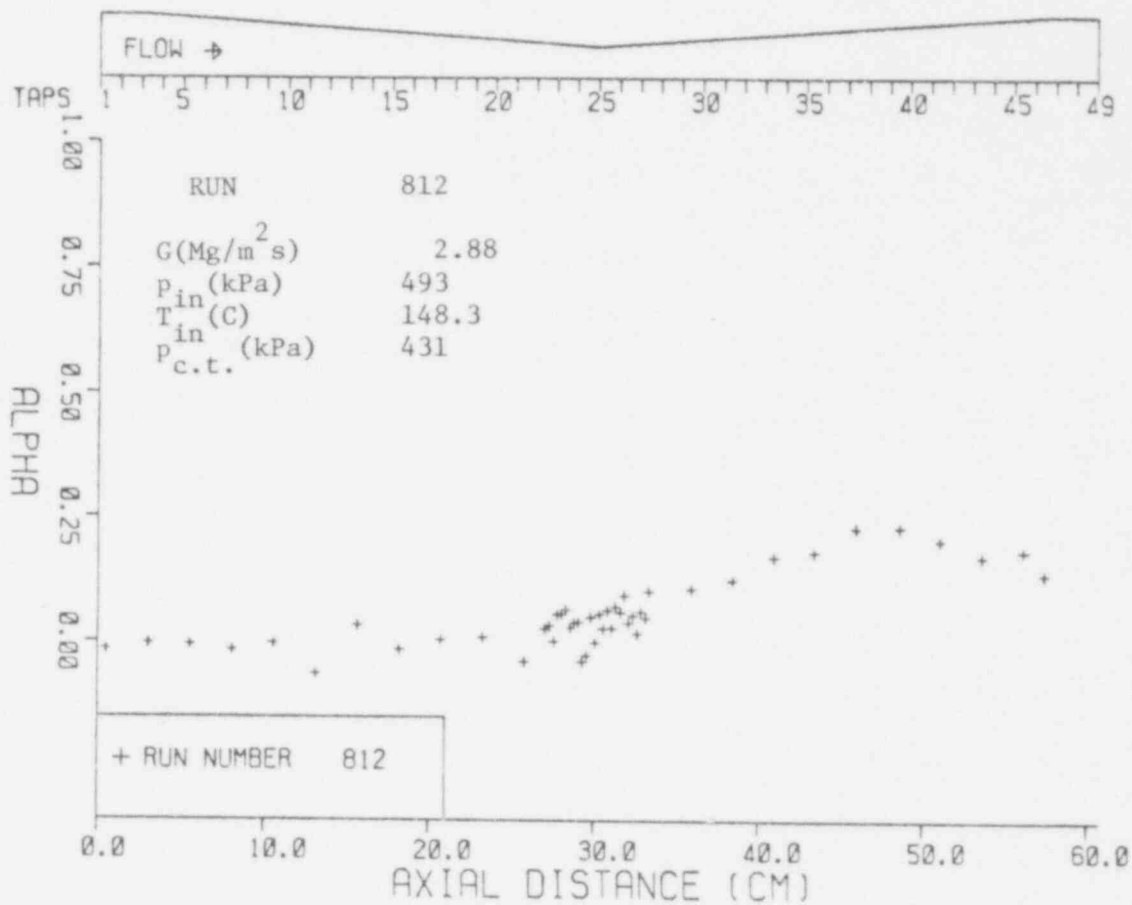
-200-

575 232

POOR ORIGINAL

BNL FLASHING FLOWS EXPERIMENT  
GAMMA DENSITOMETER DATA  
TEST SECTION # 2

LOCATION IN CM FROM TAP 49	AVERAGE NUMBER OF COUNTS IN 54 SEC	AVERAGE ALPHA	STD DEV
3.31	1027.	.14	.05
4.58	1058.	.18	.04
7.11	1087.	.17	.04
9.65	1102.	.20	.05
12.10	1147.	.23	.03
14.73	1176.	.23	.05
17.28	1174.	.18	.06
19.82	1226.	.17	.04
22.36	1208.	.12	.07
24.88	1218.	.11	.08
27.45	1270.	.10	.07
27.70	1288.	.05	.07
27.94	1315.	.06	.06
28.19	1338.	.07	.05
28.44	1376.	.05	.07
28.71	1363.	.04	.06
28.92	1369.	.09	.10
29.20	5404.	.06	.06
29.48	1332.	.07	.07
29.73	1298.	.03	.04
29.98	1270.	.06	.09
30.24	1225.	.03	.08
30.48	11880.	.05	.05
30.74	1205.	.04	.12
31.00	1266.	.05	.05
31.25	1248.	.03	.05
31.51	1258.	.04	.07
31.76	1306.	.04	.07
32.01	1320.	.04	.07
32.26	1302.	.03	.08
32.52	1308.	.06	.06
32.77	1291.	.05	.10
33.02	1269.	.05	.09
33.27	1266.	.03	.04
33.51	1279.	.03	.07
33.78	1268.	.02	.07
35.05	1172.	.04	.08
37.59	1193.	.01	.07
40.15	1148.	.00	.06
42.67	1085.	.02	.07
45.22	1095.	.03	.05
47.75	1026.	.06	.07
50.29	976.	.03	.06
52.83	971.	.02	.03
55.39	939.	.01	.06
57.91	931.	.00	.05
60.45	903.	.02	.05



-201-

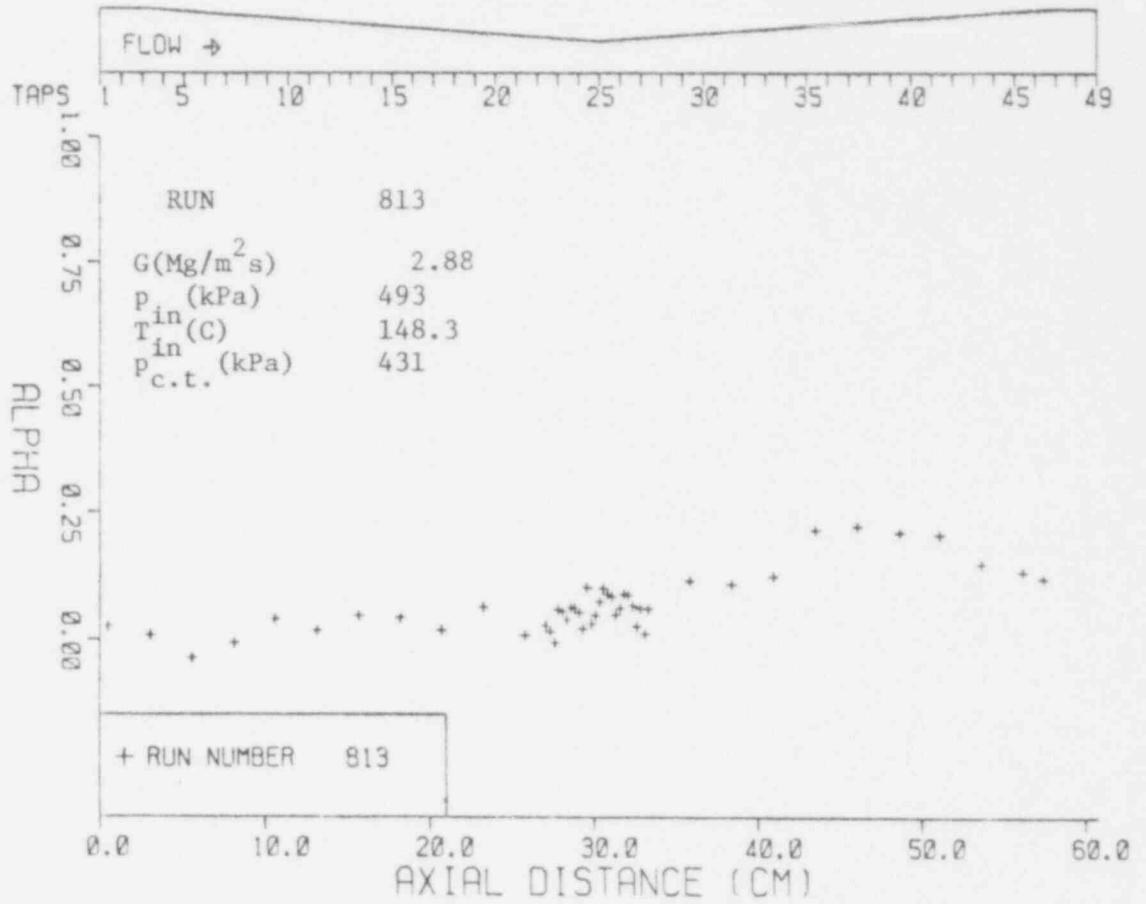
575 233

POOR ORIGINAL

BNL FLASHING FLOWS EXPERIMENT  
GAMMA DENSITOMETER DATA  
TEST SECTION # 2

RUN NUMBER 813

LOCATION IN CM FROM TAP 49	AVERAGE NUMBER OF COUNTS IN 54 SEC	AVERAGE ALPHA	STD DEV
3.31	1009.	.12	.04
4.58	1015.	.13	.03
7.11	1066.	.15	.03
9.65	1097.	.21	.04
12.10	1127.	.21	.06
14.73	1166.	.22	.04
17.28	1190.	.21	.05
19.82	1190.	.12	.06
22.36	1192.	.11	.06
24.88	1208.	.11	.07
27.45	1240.	.06	.05
27.78	1262.	.01	.06
27.94	1309.	.06	.05
28.19	1306.	.03	.05
28.44	1327.	.07	.08
28.71	1383.	.09	.07
28.92	1359.	.09	.06
29.20	1326.	.06	.05
29.48	1314.	.05	.05
29.73	1320.	.08	.05
29.98	1276.	.09	.06
30.24	1253.	.10	.07
30.48	1195.	.07	.12
30.74	1221.	.05	.08
31.00	1251.	.03	.10
31.25	1304.	.10	.12
31.51	1282.	.12	.06
31.76	1305.	.05	.08
32.01	1325.	.06	.09
32.26	1313.	.06	.07
32.52	1289.	.09	.08
32.77	1282.	.06	.06
33.02	1264.	.06	.06
33.27	1257.	.11	.08
33.53	1264.	.02	.07
33.78	1263.	.13	.07
35.05	1190.	.01	.08
37.59	1221.	.06	.10
40.15	1150.	.02	.07
42.67	1113.	.04	.06
45.22	1098.	.05	.04
47.75	1068.	.02	.04
50.29	997.	.04	.04
52.83	973.	.01	.05
55.39	915.	.04	.03
57.91	935.	.01	.06
60.45	925.	.03	.03



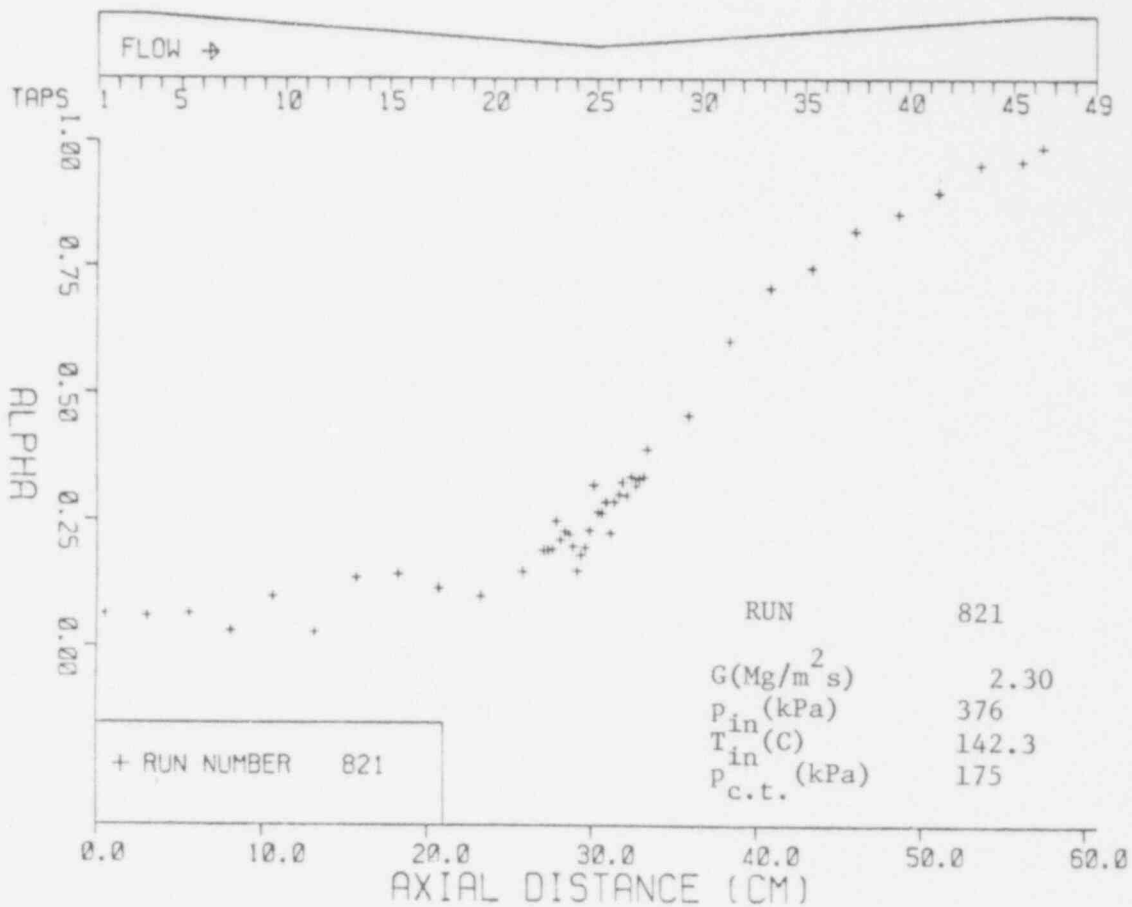
POOR ORIGINAL



BNL FLASHING FLOWS EXPERIMENT  
 GAMMA DENSITOMETER DATA  
 TEST SECTION # 2

RUN NUMBER 821

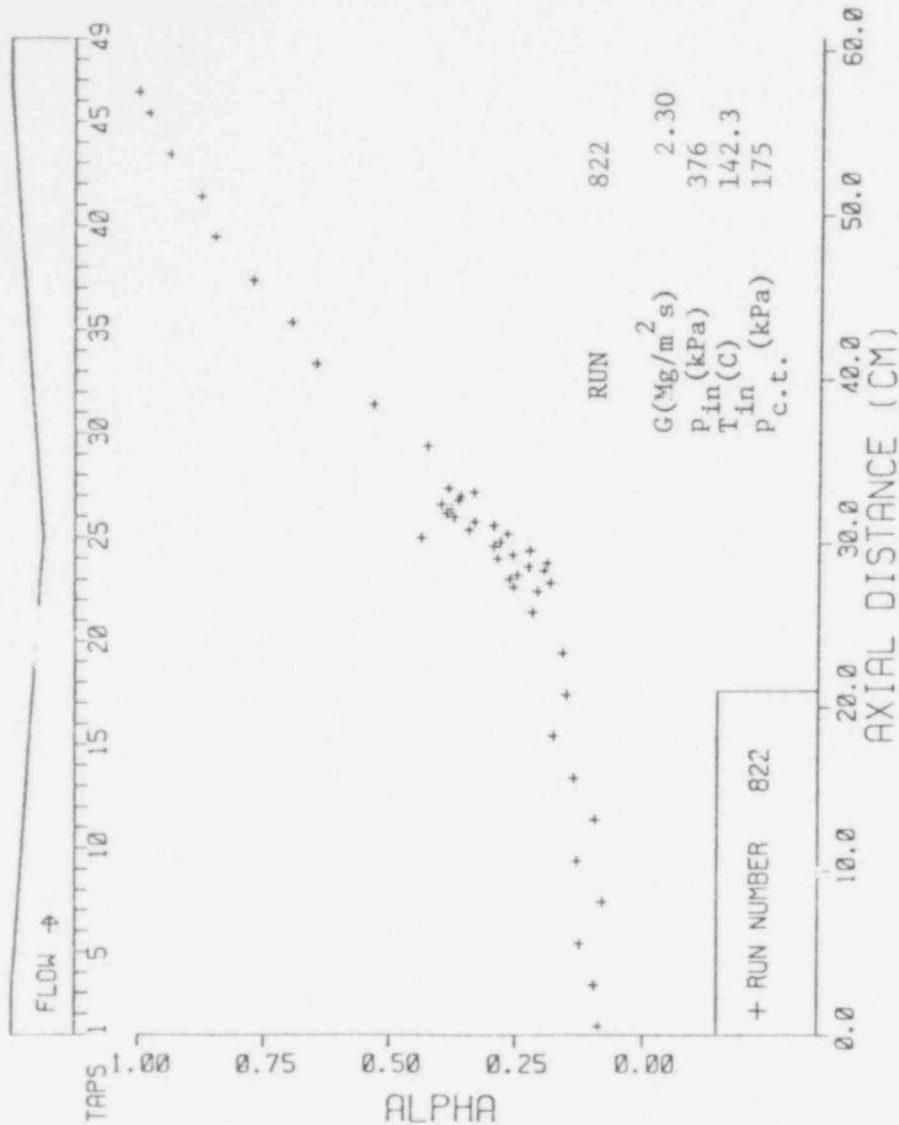
LOCATION IN CM FROM TAP 49	AVERAGE NUMBER OF COUNTS IN 54 SEC	AVERAGE ALPHA	STD DEV
3.31	1874.	.99	.02
4.58	1840.	.96	.03
7.11	1796.	.95	.02
9.65	1712.	.90	.05
12.10	1666.	.86	.05
14.73	1632.	.82	.04
17.28	1591.	.75	.06
19.82	1599.	.71	.04
22.36	1512.	.60	.12
24.88	1417.	.45	.05
27.45	1432.	.39	.04
29.70	1437.	.33	.06
27.94	1467.	.33	.08
28.19	1502.	.32	.05
28.44	1530.	.33	.06
28.71	1507.	.30	.04
28.92	1493.	.32	.05
29.20	1464.	.30	.05
29.48	1443.	.29	.07
29.73	1393.	.22	.07
29.98	1385.	.29	.06
30.24	1332.	.26	.09
30.48	1280.	.27	.05
30.74	1353.	.32	.15
31.00	1346.	.23	.07
31.25	1347.	.19	.06
31.51	1361.	.18	.05
31.76	1349.	.15	.08
32.01	1394.	.20	.06
32.26	1392.	.22	.04
32.52	1384.	.23	.06
32.77	1359.	.21	.10
33.02	1362.	.25	.10
33.27	1356.	.19	.09
33.53	1352.	.19	.08
33.78	1345.	.19	.08
35.05	1259.	.15	.05
37.59	1237.	.10	.06
40.15	1201.	.11	.05
42.67	1168.	.14	.06
45.22	1149.	.14	.05
47.75	1071.	.03	.04
50.29	1030.	.10	.07
52.83	991.	.03	.04
55.39	975.	.07	.04
57.91	966.	.06	.06
60.45	948.	.07	.05



-203-

575 235

POOR ORIGINAL

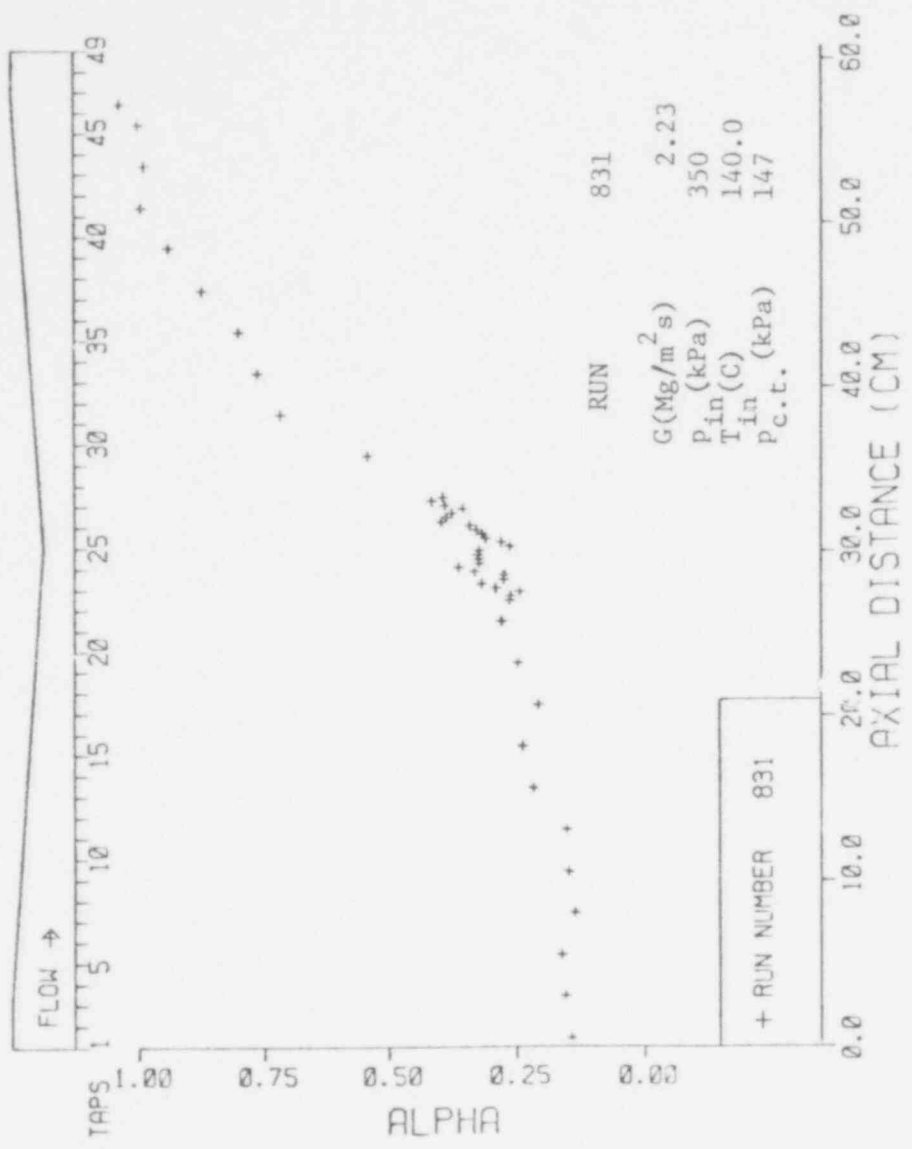


LOCATION IN CM FROM TAP 49	RUN NUMBER	AVERAGE NUMBER OF COUNTS IN 54 SEC	AVERAGE ALPHA	STD DEV
3.31	1875	1.00	1.00	.00
4.58	1852	.98	.98	.02
7.11	1769	.94	.94	.05
9.65	1678	.88	.88	.05
12.10	1648	.85	.85	.03
14.73	1578	.77	.77	.03
17.28	1538	.70	.70	.05
19.82	1541	.65	.65	.03
22.36	1453	.53	.53	.07
24.88	1389	.42	.42	.06
27.45	1421	.38	.38	.04
29.70	1427	.33	.33	.04
32.00	1475	.26	.26	.08
34.48	1522	.26	.26	.07
36.94	1559	.39	.39	.06
39.44	1548	.38	.38	.05
41.92	1522	.39	.39	.06
44.40	1527	.37	.37	.13
46.88	1461	.33	.33	.06
49.36	1409	.29	.29	.08
51.84	1326	.27	.27	.09
54.32	1359	.43	.43	.19
56.80	1324	.28	.28	.10
59.28	1370	.29	.29	.08
61.76	1354	.22	.22	.05
64.24	1394	.26	.26	.05
66.72	1409	.28	.28	.04
69.20	1381	.19	.19	.05
71.68	1387	.22	.22	.04
74.16	1359	.10	.10	.05
76.64	1370	.25	.25	.06
79.12	1362	.26	.26	.05
81.60	1343	.18	.18	.04
84.08	1343	.25	.25	.06
86.56	1348	.21	.21	.08
89.04	1299	.22	.22	.04
91.52	1264	.16	.16	.04
94.00	1216	.15	.15	.07
96.48	1183	.18	.18	.09
98.96	1144	.14	.14	.07
101.44	1109	.09	.09	.06
103.92	1044	.13	.13	.04
106.40	1019	.08	.08	.05
108.88	1010	.11	.11	.07
111.36	960	.11	.11	.07
113.84	931	.07	.07	.04
116.32	938	.09	.09	.04

POOR ORIGINAL

RNL FLASHING FLOWS EXPERIMENT  
 GAMMA DEPOSITIONER DATA  
 TEST SECTION # 2

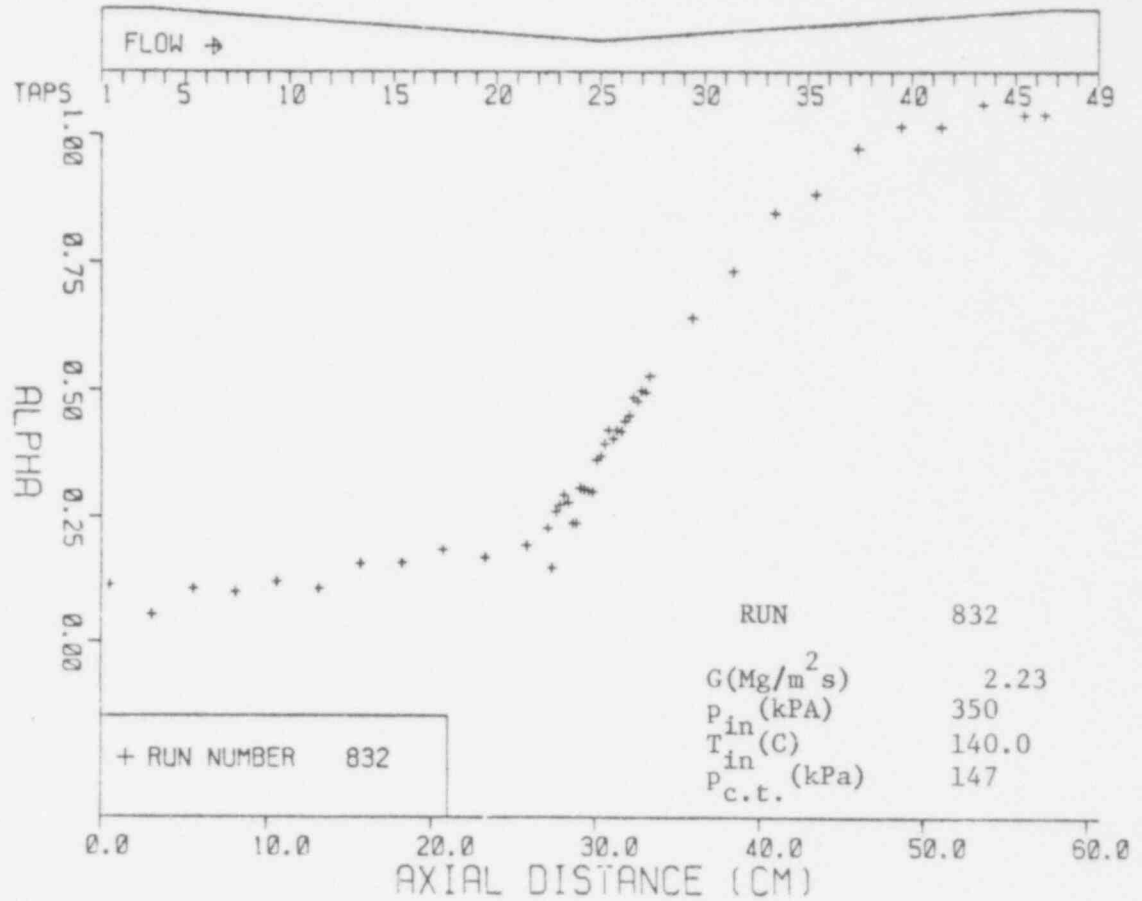
LOCATION IN CW FROM TAP #9	RUN NUMBER	AVERAGE COUNTS IN 54 SEC	AVERAGE ALPHA	STD DEV
3.31	1925	1.00	1.00	.02
4.58	1890	.99	1.00	.02
7.11	1826	.99	.99	.03
9.65	1808	.99	.99	.03
12.10	1783	.94	.94	.04
14.73	1672	.87	.87	.03
17.28	1630	.80	.80	.07
19.82	1635	.80	.80	.04
22.36	1588	.72	.72	.05
24.84	1467	.54	.54	.05
27.45	1427	.39	.39	.07
27.93	1476	.41	.41	.08
27.94	1494	.39	.39	.08
28.19	1515	.35	.35	.05
28.44	1544	.37	.37	.03
28.71	1552	.38	.38	.06
28.92	1527	.39	.39	.08
29.20	1479	.34	.34	.05
29.48	1457	.32	.32	.05
29.73	1435	.31	.31	.08
29.98	1388	.31	.31	.06
30.24	1301	.28	.28	.05
30.48	1269	.26	.26	.07
30.74	1344	.32	.32	.05
31.00	1385	.32	.32	.08
31.25	1403	.32	.32	.06
31.51	1479	.32	.32	.03
31.76	1459	.36	.36	.08
32.01	1411	.33	.33	.09
32.26	1399	.27	.27	.06
32.52	1466	.27	.27	.07
32.77	1377	.29	.29	.04
33.02	1374	.29	.29	.08
33.27	1362	.24	.24	.10
33.53	1377	.26	.26	.07
33.78	1377	.26	.26	.12
35.05	1373	.28	.28	.11
37.59	1312	.24	.24	.06
41.05	1247	.21	.21	.06
45.57	1193	.24	.24	.05
47.35	1141	.22	.22	.07
50.59	1083	.15	.15	.06
52.83	1053	.14	.14	.05
55.90	1035	.16	.16	.06
57.91	1035	.16	.16	.05
60.45	996	.14	.14	.05



POOR ORIGINAL

BNL FLASHING FLOWS EXPERIMENT  
 GAMMA DENSITOMETER DATA  
 TEST SECTION # 2

LOCATION IN CM FROM TAP 49	AVERAGE NUMBER OF COUNTS IN 54 SEC	AVERAGE ALPHA	STD DEV
3.31	1923.	1.04	.03
4.58	1924.	1.04	.03
7.11	1905.	1.06	.04
9.65	1825.	1.02	.02
12.10	1917.	1.02	.03
14.73	1760.	.97	.04
17.28	1696.	.88	.06
19.82	1698.	.85	.04
22.36	1593.	.73	.07
24.88	1532.	.64	.04
27.45	1507.	.53	.05
27.70	1517.	.50	.05
27.94	1560.	.50	.10
28.19	1587.	.48	.09
28.44	1607.	.49	.08
28.71	1586.	.45	.07
28.92	1545.	.44	.07
29.20	1521.	.42	.08
29.48	1506.	.42	.04
29.73	1478.	.40	.06
29.98	1448.	.42	.06
30.24	1383.	.39	.08
30.48	1316.	.37	.10
30.74	1359.	.36	.12
31.00	1366.	.30	.08
31.25	1386.	.30	.07
31.51	1412.	.30	.07
31.76	1412.	.31	.06
32.01	1400.	.24	.05
32.26	1385.	.24	.07
32.52	4487.	.28	.10
32.77	1386.	.29	.07
33.02	1360.	.27	.07
33.27	1377.	.26	.07
33.53	71077.	.15	.13
33.78	1350.	.23	.08
35.05	1269.	.19	.10
37.59	1261.	.17	.07
40.15	1226.	.18	.04
42.67	1162.	.16	.04
45.22	1148.	.15	.08
47.75	1106.	.11	.04
50.29	1031.	.12	.05
52.81	1024.	.10	.04
55.39	990.	.11	.07
57.91	949.	.06	.05
60.45	969.	.11	.03



-206-

575 238

POOR ORIGINAL

DISTRIBUTION LIST

G. Bagchi, NRC  
D. Basdekas, NRC  
V. Benaroya, NRC  
C. Burger, NRC  
R. T. Curtis, NRC  
S. Fabric, NRC  
D. Fischer, NRC  
Y. Y. Lau, NRC  
W. Y. Kato, BNL  
C. N. Kelber, NRC  
H. J. Kouts, BNL  
R. Mattson, NRC  
A. W. Serkiz, NRC  
L. Shao, NRC  
M. Silberberg, NRC  
L. Thompson, NRC  
H. Todosow, BNL  
L. S. Tong, NRC  
R. W. Wright, NRC  
N. Zuber, NRC

BNL RSP Division Heads  
BNL RSP Group Leaders  
BNL RSE Modeling Group

U.S. NRC Division of  
Technical Information  
and Control

POOR ORIGINAL