

ATTACHMENT V

Consumers Power Company
Palisades Plant
Docket 50-255

PRESSURE RESPONSE EFFECT OF VLTOP
WITH REPLACEMENT PORVs
(EA-FC-809-13, Rev. 1)

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TITLE: PRESSURE RESPONSE EFFECTS OF VLTOP WITH REPLACEMENT PORVs

PURPOSE:

ESTABLISH PERMISSABLE VLTOP ACTUATION SET POINTS

PROCEDURE UTILIZED:

HAND CALCULATIONS

SIMILARITIES WITH PREVIOUS DESIGNS:

BOTH MASS ADDITIONS AND V_f CHANGES WERE ADDRESSED IN PREVIOUS ANALYSES, BUT PREVIOUS ANALYSES ASSUMED A CONSTANT K , BULK MODULUS OF ELASTICITY.

SUMMARY OF RESULTS: See CURVES ATTACHED TO PARTS I & II

SPECIAL MEDIA ATTACHED (DRAWINGS, MICROFICHE, ETC)

NO YES - LIST OF ATTACHMENTS INCLUDED

FSAR UPDATE REQUIRED: NO YES UPDATE ATTACHED OR SHOULD BE COMPLETED AS PART OF FC PACKAGE

UPDATE ASSIGNED TO: _____

REQUIRED COMPLETION DATE: _____

J. A. ... 19 Sept 1989
PREPARED BY Date

J. A. ... 19/20/89
PREPARER Date
APPROVED BY

Timothy C. Duffey 9/20/89
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ENGINEERING ANALYSIS

Title: Pressure Response Effects of VLTOP with Replacement PORVs

Methodology:

The analysis is completed in four parts, described below. One part determines pressure overshoot, another the PORV flows, another the recommended LTOP set points, and the last, the Tech Specs limit.

Part I calculates the rate at which Pzr pressure would increase for permissible heating rates (PCS and Pzr), and mass addition rates. It also calculates an equivalent gpm for all effects, for use in Part III - Valve Opening Requirements. Mass addition rates both with and without HPSI are calculated over the 230 to 350 degree PCS temperature range.

Part II calculates the water flow for a single PORV to open full stroke, for use in Part III and Part IV.

Part III calculates the Appendix G pressure limits for PCS temperatures with allowance for temperature and pressure errors of 5 degrees and 30 psi respectively, and an allowance for pressure overshoot. These are the LTOP setpoints. The setpoints are plotted, and then a new plot of a smooth curve is prepared which envelopes all of the set points. This second curve is the recommended LTOP set point curve.

Part IV calculates the Appendix G pressure limits for PCS temperatures without temperature and pressure error, but with allowance for pressure overshoot. These values are plotted, and produce the LTOP Tech Specs Limit curve (3-4 in the T.S. change request).

During the preparation and review of this analysis, several questions were raised, and answered. The more significant of these are included below:

1) WHAT CONSERVATISMS ARE INCLUDED IN THE ANALYSIS?

- a) The longest PORV full stroke time was utilized in calculating time until required flow, for all cases, even though Pzr liquid would have to be saturated to produce such a stroke time. Times with subcooled liquid are computed to be substantially shorter.
- b) PORV flow figure used was that for only 310 psia in the pressurizer, regardless of LTOP set point. Further, PORV backpressure was assumed to be 115 psia continuously, even though it will likely be much lower initially, and cannot be sustained at that level due to the quench tank rupture disc's 90 psig set point.

- c) Pressurizer heating rate was assumed to be 200 deg/hr, as permitted, but actual maximum heating rate when pressurizer is water-solid is substantially lower.
- d) The Bulk Modulus of Elasticity, k, was not recalculated for every temperature above 200 degrees, but rather was 'stepped' down, such that over much of the temperature range it is higher than actual, resulting in calculation of a higher than actual rate of pressure increase.
- e) No PORV flow is assumed to occur until the valve is full open; ie, flow is stepped, not ramped.
- f) PCS volume is assumed to be that resulting from 29.3% average steam generator tube plugging, worsening the pressure increase rate over that with the current level of plugging (~25.5%)

2) WHY ARE THE POTENTIAL MEASUREMENT ERRORS NOT INCLUDED IN THE LTOP TECH SPECS LIMIT CURVE?

The T.S. curve represents the pressure at which the PORV must be actuated in order to prevent exceeding the Appendix G limit, considering the pressure overshoot during the time it takes for the valve to open. The amount by which the set point must be reduced below this value to offset potential error, drift, etc. may vary under the influence of calibration temperature, and instrument sensitivity. The requirement is that LTOP circuitry set point be reached at the same time or before the T.S. limiting pressure is reached. With this approach, surveillance tests should never find an LTOP set point in excess of the T.S. limit.

3) WHY IS PROTECTION OF THE SDC SYSTEM NO LONGER PROVIDED BY THE PORVS?

The LTOP set point which would be necessary to protect the SDC system would be too low.

- . SDC is designed for 500 psig
- . The LPSI pumps can add as much as 197 psi to the system pressure
- . The LPSI pump discharge is @ ~571.5 elev.
- . Pzr pressure (LTOP pressure input) is measured @ ~650 elev.
- . Elevation difference adds ~34 psi to indicated system pressure
- . Potential pressure error of LTOP instrumentation (narrow range) is ~24 psi

The set point of LTOP to protect SDC system would therefore have to be $(500 \text{ psig} + 15) - 197 - 34 - 24 = 260 \text{ psia}$. Actual operating pressure would have to be reduced below this value to prevent inadvertent opening of PORVs, and to keep alarm (LTOP) cleared.

SDC system RVs will provide adequate protection against charging without letdown (133 gpm) in coincidence with PCS heating @ 40 deg/hr (25 gpm) and Pzr heating @ 60 deg/hr (9 gpm). RVs are 3164 (133 gpm), 3162 (5 gpm), 0402 (15 gpm), and 0403 (15 gpm). ER-PAL-89-040 will resolve their set points to account for elevation head and ensure SDC overpressure protection without reliance on the PORVs.

- 4) LTOP limit is shown a single curve for heating and cooling. Which is limiting?

Based on revised Appendix G limits (through $1.8E19 \text{ nvt}$), and on permissible rate of change, the LTOP limit is set by cooling constraints below $\sim 280 \text{ deg F}$, and by heating constraints above $\sim 290 \text{ deg F}$. The exact crossover point depends upon whether or not instrument error allowances are included, and is also affected by the assumed heating or cooling rate. For the rates assumed (maximum permissible rates for the PCS temperature), all pressure limits were from the 1/4t Appendix G calculations. Future changes in permissible rates, or in Appendix G limits could result in the 3/4t values being more limiting. Therefore, any change in permissible heating/cooling rates, or in vessel fluence, should prompt investigations into the possibility of the 3/4t values being more limiting, and into a shift in the crossover point in which values are limiting (heating or cooling).

Part I - Pressure Increase Rates for Various PCS Heating Rates and Pump Start Combinations

Objective:

Determine the rate of Pressurizer pressure increase for inadvertent pump starts when PCS is water-solid as input to calculate Pzr pressure overshoot during LTOP actuation time.

Analysis Input:

- a) Pzr heating rate = 200 degrees/hour.
- b) PCS heating rates = 20 deg/hr up to 170 deg F. (ref 4)
40 deg/hr from 170 to 250 deg F.
60 deg/hr from 250 to 350 deg F.
100 deg/hr from 350 to 532 deg F.

c) Rate of Pzr pressure increase, $\text{psi/sec} = K(-dV/V)$, from ref 1, where $V = \text{PCS volume} = 10,311.7\text{ft}^3$, from ref 2 & 3, and
 $dV = \text{Swell and mass additions, converted to ft}^3/\text{sec}$, and
 $K = \text{Bulk modulus of elasticity for water (see attachment 1)}$

d) dV is calculated for Swell from the relationship

$dV = (V_f - V_f') / V_f * V_{pcs} / t$ or $(V_f - V_f') / V_f * V_{pzr} / t$,
where $V_f = \text{fluid specific volume @ temp of interest}$, and
 $V_f' = \text{fluid specific volume @ temp of interest} + 10 \text{ deg}$, and
 V_{pcs} , or $V_{pzr} = \text{the affected volume}$, and
 $t = \text{the elapsed time for the temperature change, in seconds}$

$V_{pcs} = \text{PCS volume} - \text{Pzr volume} = 8,808\text{ft}^3$, from ref 2

$V_{pzr} = \text{Pressurizer volume} = 1,503.7$, from ref 3

e) dV is calculated for mass additions from the relationship

dV_{chg} , or $dV_{hpsi} = \text{gpm} / \text{gal/ft}^3 / \text{sec/min} = \text{ft}^3/\text{sec}$,

where $dV_{chg} = \text{charging flow} = 133\text{gpm}$, and
 $dV_{hpsi} = \text{High Pressure Safety Injection Flow from ref 6}$, and
 $\text{gal/ft}^3 = 7.48$, and
 $\text{sec/min} = 60$

f) HPSI pumps delivery as a function of Pzr pressure is taken from reference 6.

g) Constants used in the analyses are:

$A = V_{pcs} / t = 8,808 / 1,800 = 4.8933... \text{ft}^3/\text{sec}$ over the range of
50 to 170 deg F

$= 8,808 / 900 = 9.7866... \text{ft}^3/\text{sec}$ for 170 to 250 deg

$= 8,808 / 600 = 14.68 \text{ft}^3/\text{sec}$ for 250 to 350 deg

$= 8,808 / 360 = 24.466... \text{ft}^3/\text{sec}$ for 350 & up

$B = V_{pzr} / t = 1,503.7 / 180 = 8.3539$ for all temperatures

$C = K / V = 305,000 / 10,311.7 = 29.578052 \text{psi/ft}^3$ @ 50 deg F.
[C is recalculated each 10 deg F from 50 to 200 deg F, then @ 50 deg C intervals; see attachment 1]

$K = \text{Bulk modulus of elasticity for water; see attachment 1}$

Assumptions:

- a) All HPSI pumps are disabled @ PCS temperatures <260 deg F (ref 4).
- b) Steam Generator tube plugging will not reduce PCS volume below 10,311.7 ft³, which corresponds to 29.3% average fraction of tubes plugged (ref 2). [PCS volume with 23.68 & 24.49% SG 1 & 2 plugging respectively = 10,403.95ft³]
- c) Inadvertent start of charging is in coincidence with isolation of letdown, maximum Pzr heating rate, and maximum PCS heating rates.
- d) Inadvertent start of HPSI is in coincidence with inadvertent start of charging, maximum Pzr heating, and maximum PCS heating.
- e) PCS is water-solid at beginning of transient.
- f) PCS heating rates are the maximums permitted (ref 4).
- g) No reduction in mass addition rate is taken as Pzr pressure rises above initial pressure.
- h) Initial pressures are taken as equal to the shutdown cooling LTOP set point from 50 to 350 degrees, then taken as over 80 psi less than expected LTOP set points, to maximize HPSI delivery.
- i) Pressurizer fluid is taken as being in equilibrium with the PCS until both are heated to 200 deg F; then, Pzr fluid is taken as being near saturation, to maximize volume change from Pzr heating.
- j) Delivery from two HPSI pumps to the PCS is twice that from one HPSI pump.

Constants on this page: A = 4.0933 B = 9.3539 C = 29.8484 K = 307,788
30,6135 315,675
31,2702 322,449

PCS temperature 50 Vf @ 310 psia = .01601 Vf' @ 60 & 310 psia = .01602
 Pzr temp 50 Vf @ 310 psia = .01601 Vf' @ & psia =

dVhpsi = N/A gpm / 7.48 / 60 = ft³ / sec

dVchg = 133 gpm / 7.48 / 60 = .2963 ft³ / sec

dVpcs = .00001 / .01601 * A = .0031 ft³ / sec

dVpzc = .00001 / .01601 * B = .0052 ft³ / sec

dVtot = .3046 ft³ / sec

RATE of Pzr Press rise =
dVtot * C = .3046 * C =

9.0918 psi / sec

Equivalent gpm = (7.48 * 60 * .3046 ft³) = 136.7 gpm

PCS temperature 60 Vf @ 310 psia = .01602 Vf' @ 70 & 310 psia = .01603
 Pzr temp 60 Vf @ 310 psia = Vf' @ & psia =

dVhpsi = N/A gpm / 7.48 / 60 = ft³ / sec

dVchg = 133 gpm / 7.48 / 60 = .2963 ft³ / sec

dVpcs = .00001 / .01602 * A = .0031 ft³ / sec

dVpzc = .00001 / .01602 * B = .0052 ft³ / sec

dVtot = .3046 ft³ / sec

RATE of Pzr Press rise =
dVtot * C = .3046 * C =

9.3249 psi / sec

Equivalent gpm = (7.48 * 60 * .3046 ft³) = 136.7 gpm

PCS temperature 70 Vf @ 310 psia = .01603 Vf' @ 80 & 310 psia = .01606
 Pzr temp 70 Vf @ psia = Vf' @ & psia =

dVhpsi = N/A gpm / 7.48 / 60 = ft³ / sec

dVchg = 133 gpm / 7.48 / 60 = .2963 ft³ / sec

dVpcs = .00003 / .01603 * A = .0092 ft³ / sec

dVpzc = .00003 / .01603 * B = .0156 ft³ / sec

dVtot = .3211 ft³ / sec

RATE of Pzr Press rise =
dVtot * C = .3211 * C =

10.0409 psi / sec

Equivalent gpm = (7.48 * 60 * .3211 ft³) = 144.1257 gpm

NOTES:

Constants on this page: A = 4.8933 B = 8.3539 C = 31.4939 K = 324,756
31.7177 327,063
31,9416 329,372

PCS temperature 80° Vf @ 310 psia = .01606 Vf' @ 90° & 310 psia = .01608
 Pzr temp 80° Vf @ ___ psia = ___ Vf' @ ___ & ___ psia = ___

dVhpsi = N/A gpm/7.48/60 = ___ ft³/sec

dVchg = 133 gpm/7.48/60 = .2963 ft³/sec

dVpcs = .000024 * .01606 * A = .0061 ft³/sec

RATE of Pzr Press rise =
dVtot * C = .3128 * C =

dVpzr = .000024 * .01606 * B = .0104 ft³/sec

9.8513 psi/sec

dVtot = .3128 ft³/sec

Equivalent gpm = (7.48 * 60 * .3128 ft³) = 140.386 gpm

PCS temperature 90° Vf @ 310 psia = .01608 Vf' @ 100° & 310 psia = .01611
 Pzr temp 90° Vf @ ___ psia = ___ Vf' @ ___ & ___ psia = ___

dVhpsi = N/A gpm/7.48/60 = ___ ft³/sec

dVchg = 133 gpm/7.48/60 = .2963 ft³/sec

dVpcs = .000027 * .01608 * A = .0091 ft³/sec

RATE of Pzr Press rise =
dVtot * C = .3210 * C =

dVpzr = .000027 * .01608 * B = .0156 ft³/sec

10.1814 psi/sec

dVtot = .3210 ft³/sec

Equivalent gpm = (7.48 * 60 * .3210 ft³) = 144.058 gpm

PCS temperature 100° Vf @ 310 psia = .01611 Vf' @ 110° & 310 psia = .01615
 Pzr temp 100° Vf @ ___ psia = ___ Vf' @ ___ & ___ psia = ___

dVhpsi = N/A gpm/7.48/60 = ___ ft³/sec

dVchg = 133 gpm/7.48/60 = .2963 ft³/sec

dVpcs = .000041 * .01611 * A = .0121 ft³/sec

RATE of Pzr Press rise =
dVtot * C = .3291 * C =

dVpzr = .000041 * .01611 * B = .0207 ft³/sec

10.5120 psi/sec

dVtot = .3291 ft³/sec

Equivalent gpm = (7.48 * 60 * .3291 ft³) = 147.719 gpm

NOTES:

Constants on this page: A = 4.8933 B = 8.2539 C = 32.0995 K = 331,679
32.3091 333,987
32.1006 331,012

PCS temperature 110° Vf @ 310 psia = .01615 Vf' @ 120° & 310 psia = .01619
 Fzr temp 110° Vf @ ___ psia = ___ Vf' @ ___ & ___ psia = ___

dVhpsi = N/A gpm/7.48/60 = ___ ft³/sec

dVchg = 133 gpm/7.48/60 = .2963 ft³/sec

dVpcs = .000041 * .01615 * A = .0121 ft³/sec

RATE of Fzr Press rise =
dVtot * C = .3291 * C =

dVpZR = .000041 * .01615 * B = .0207 ft³/sec

10.5856 psi/sec

dVtot = .3291 ft³/sec

Equivalent gpm = (7.48 * 60 * .3291 ft³) = 147.6959 gpm

PCS temperature 120° Vf @ 310 psia = .01619 Vf' @ 130° & 310 psia = .01623
 Fzr temp 120° Vf @ ___ psia = ___ Vf' @ ___ & ___ psia = ___

dVhpsi = N/A gpm/7.48/60 = ___ ft³/sec

dVchg = 133 gpm/7.48/60 = .2963 ft³/sec

dVpcs = .000041 * .01619 * A = .0121 ft³/sec

RATE of Fzr Press rise =
dVtot * C = .3290 * C =

dVpZR = .000041 * .01619 * B = .0206 ft³/sec

10.656 psi/sec

dVtot = .3290 ft³/sec

Equivalent gpm = (7.48 * 60 * .3290 ft³) = 147.673 gpm

PCS temperature 130° Vf @ 310 psia = .01623 Vf' @ ___ & 310 psia = .01628
 Fzr temp 130° Vf @ ___ psia = ___ Vf' @ ___ & ___ psia = ___

dVhpsi = N/A gpm/7.48/60 = ___ ft³/sec

dVchg = 133 gpm/7.48/60 = .2963 ft³/sec

dVpcs = .0000251 * .01623 * A = .0151 ft³/sec

RATE of Fzr Press rise =
dVtot * C = .3371 * C =

dVpZR = .0000251 * .01623 * B = .0257 ft³/sec

10.8211 psi/sec

dVtot = .3371 ft³/sec

Equivalent gpm = (7.48 * 60 * .3371 ft³) = 151.2905 gpm

NOTES:

Constants on this page: A = 4.8933 B = 8.3539 C = 31.8121 K = 328,037
 31.5236 325,062
 31.2350 322,086

PCS temperature 140° Vf @ 310 psia = .01628 Vf @ 150° & 310 psia = .01633
 Pzr temp 140° Vf @ ___ psia = ___ Vf @ ___ & ___ psia = ___

dVhpsi = N/A gpm/7.48/60 = ___ ft³/sec

dVchg = 133gpm/7.48/60 = .2963ft³/sec

dVpcs = .00005/.01628*A = .0150ft³/sec

RATE of Pzr Press rise =
dVtot*C = .3370*C =

dVpzr = .00005/.01628*B = .0257ft³/sec

10.7207 psi/sec

dVtot = .3370 ft³/sec

Equivalent gpm = (7.48*60*.3370ft³) = 151.2263 gpm

PCS temperature 150° Vf @ 310 psia = .01633 Vf @ 160° & 310 psia = .01638
 Pzr temp 150° Vf @ ___ psia = ___ Vf @ ___ & ___ psia = ___

dVhpsi = N/A gpm/7.48/60 = ___ ft³/sec

dVchg = 133gpm/7.48/60 = .2963ft³/sec

dVpcs = .00005/.01633*A = .0150ft³/sec

RATE of Pzr Press rise =
dVtot*C = .3369*C =

dVpzr = .00005/.01633*B = .0256ft³/sec

10.6203 psi/sec

dVtot = .3369 ft³/sec

Equivalent gpm = (7.48*60*.3369 ft³) = 151.191 gpm

PCS temperature 160° Vf @ 310 psia = .01638 Vf @ 170° & 310 psia = .01644
 Pzr temp 160° Vf @ ___ psia = ___ Vf @ ___ & ___ psia = ___

dVhpsi = N/A gpm/7.48/60 = ___ ft³/sec

dVchg = 133gpm/7.48/60 = .2963ft³/sec

dVpcs = .00006/.01638*A = .0179 ft³/sec

RATE of Pzr Press rise =
dVtot*C = .3448*C =

dVpzr = .00006/.01638*B = .0306 ft³/sec

10.7698 psi/sec

dVtot = .3448 ft³/sec

Equivalent gpm = (7.48*60*.3448 ft³) = 154.7462 gpm

NOTES:

Constants on this page: A = 9.7866 B = 8.3539 C = 30.9465 K = 319,111
30.6580 316,136
30.3695 313,161

PCS temperature 170° Vf @ 310 psia = .01644 Vf @ 100° & 310 psia = .01649
Pzr temp 170° Vf @ ___ psia = ___ Vf @ ___ & ___ psia = ___

dVhpsi = N/A gpm / 7.48 / 60 = ___ ft³ / sec

dVchg = 133 gpm / 7.48 / 60 = .2963 ft³ / sec

1) dVpcs = .000051 * .01644 * A = .0298 ft³ / sec

RATE of Pzr Press rise =
dVtot * C = .3515 * C =

dVpzr = .000051 * .01644 * B = .0254 ft³ / sec

10.877 psi / sec

dVtot = .3515 ft³ / sec

Equivalent gpm = (7.48 * 60 * .3515 ft³) = 157.7564 gpm

PCS temperature 180° Vf @ 310 psia = .01649 Vf @ 190° & 310 psia = .01656
Pzr temp 180° Vf @ ___ psia = ___ Vf @ ___ & ___ psia = ___

dVhpsi = N/A gpm / 7.48 / 60 = ___ ft³ / sec

dVchg = 133 gpm / 7.48 / 60 = .2963 ft³ / sec

dVpcs = .000071 * .01649 * A = .0415 ft³ / sec

RATE of Pzr Press rise =
dVtot * C = .3733 * C =

dVpzr = .000071 * .01649 * B = .0355 ft³ / sec

11.4569 psi / sec

dVtot = .3733 ft³ / sec

Equivalent gpm = (7.48 * 60 * .3733 ft³) = 167.5206 gpm

PCS temperature 190° Vf @ 310 psia = .01656 Vf @ 200° & 310 psia = .01662
Pzr temp 190° Vf @ ___ psia = ___ Vf @ ___ & ___ psia = ___

dVhpsi = N/A gpm / 7.48 / 60 = ___ ft³ / sec

dVchg = 133 gpm / 7.48 / 60 = .2963 ft³ / sec

dVpcs = .000061 * .01656 * A = .0355 ft³ / sec

RATE of Pzr Press rise =
dVtot * C = .3621 * C =

dVpzr = .000061 * .01656 * B = .0303 ft³ / sec

10.9968 psi / sec

dVtot = .3621 ft³ / sec

Equivalent gpm = (7.48 * 60 * .3621 ft³) = 162.496 gpm

NOTES: 1) Increased PCS heating rate from 20/hr to 40/hr

Constants on this page: A = 9.7867 B = 8.3539 C = 30.0810 K = 310,186
29.4131 303,299

PCS temperature 200° Vf @ 310 psia = .01662 Vf @ 210° & 310 psia = .01669
 Pzr temp 410° Vf @ 310 psia = .01878 Vf @ 420° & 310 psia = .01893

dVhpsi = N/A gpm / 7.48 / 60 = ft³/sec

dVchg = 133 gpm / 7.48 / 60 = .2963 ft³/sec

dVpcs = .000071 * .01662 * A = .0412 ft³/sec

RATE of Pzr Press rise =
dVtot * C = .4042 * C =

dVpzr = .000151 * .01878 * B = .0667 ft³/sec

12.1587 psi/sec

dVtot = .4042 ft³/sec

Equivalent gpm = (7.48 * 60 * .4042 ft³) = 181.419 gpm

PCS temperature 210° Vf @ 310 psia = .01669 Vf @ 220° & 310 psia = .01676
 Pzr temp 410° Vf @ 310 psia = .01878 Vf @ 420° & 310 psia = .01893

dVhpsi = N/A gpm / 7.48 / 60 = ft³/sec

dVchg = 133 gpm / 7.48 / 60 = .2963 ft³/sec

dVpcs = .000071 * .01669 * A = .0410 ft³/sec

RATE of Pzr Press rise =
dVtot * C = .4040 * C =

dVpzr = .000151 * .01878 * B = .0667 ft³/sec

11.8843 psi/sec

dVtot = .4040 ft³/sec

Equivalent gpm = (7.48 * 60 * .4040 ft³) = 181.336 gpm

PCS temperature 220° Vf @ 310 psia = .01676 Vf @ 230° & 310 psia = .01683
 Pzr temp 410° Vf @ 310 psia = .01878 Vf @ 420° & 310 psia = .01893

dVhpsi = N/A gpm / 7.48 / 60 = ft³/sec

dVchg = 133 gpm / 7.48 / 60 = .2963 ft³/sec

dVpcs = .000071 * .01676 * A = .0409 ft³/sec

RATE of Pzr Press rise =
dVtot * C = .4039 * C =

dVpzr = .000151 * .01878 * B = .0667 ft³/sec

11.8792 psi/sec

dVtot = .4039 ft³/sec

Equivalent gpm = (7.48 * 60 * .4039 ft³) = 181.259 gpm

NOTES: D Pzr Temp assumed @ near saturation

Constants on this page: A = 9.7867 B = 8.3539 C = 29.4131 K = 303,299
14.68

PCS temperature 230° Vf @ 310 psia = .0683 Vf' @ 240° & 310 psia = .01691
Pzr temp 410° Vf @ 310 psia = .01878 Vf' @ 420° & 310 psia = .01883

dVhpsi = N/A gpm/7.48/60 = _____ ft3/sec

dVchg = 133gpm/7.48/60 = .2963ft3/sec

dVpcs = .00008/.01691 * A = .0463 ft3/sec

RATE of Pzr Press rise =
dVtot * C = .4093 * C =

dVpzr = .000151/.01878 * B = .0667 ft3/sec

12.0417 psi/sec

dVtot = .4093 ft3/sec

Equivalent gpm = (7.48*60*.4093 ft3) = 183.78³⁶ gpm

PCS temperature 240° Vf @ 310 psia = .01691 Vf' @ 250° & 310 psia = .01699
Pzr temp 410° Vf @ 310 psia = .01878 Vf' @ 420° & 310 psia = .01893

dVhpsi = N/A gpm/7.48/60 = _____ ft3/sec

dVchg = 133gpm/7.48/60 = .2963ft3/sec

dVpcs = .00008/.01691 * A = .0463 ft3/sec

RATE of Pzr Press rise =
dVtot * C = .4093 * C =

dVpzr = .000151/.01878 * B = .0667 ft3/sec

12.0308 psi/sec

dVtot = .4093 ft3/sec

Equivalent gpm = (7.48*60*.4093 ft3) = 183.69³⁸ gpm

PCS temperature 250° Vf @ 310 psia = .01699 Vf' @ 260° & 310 psia = .01707
Pzr temp 410° Vf @ 310 psia = .01878 Vf' @ 420° & 310 psia = .01883

dVhpsi = N/A gpm/7.48/60 = _____ ft3/sec

dVchg = 133gpm/7.48/60 = .2963ft3/sec

1) dVpcs = .00008/.01699 * A = .0691 ft3/sec

RATE of Pzr Press rise =
dVtot * C = .4321 * C =

dVpzr = .000151/.01878 * B = .0667 ft3/sec

12.7094 psi/sec

dVtot = .4321 ft3/sec

Equivalent gpm = (7.48*60*.4321 ft3) = 193.92⁶⁵ gpm

NOTES:

1) Begin heating PCS @ 60°/hr; A = 14.68

Constants on this page: A = 14.68 B = 8.3539 C = 29.431 K = 303.299

PCS temperature 260° Vf @ 310 psia = .01707 Vf @ 270° & 310 psia = .01716
Pzr temp 410° Vf @ 310 psia = .01978 Vf @ 420° & 310 psia = .01993

dVhpsi = $\frac{1,220 \text{ gpm}}{7.48/60} = 2.7104 \text{ ft}^3/\text{sec}$ 1)

dVchg = $\frac{133 \text{ gpm}}{7.48/60} = .2963 \text{ ft}^3/\text{sec}$

dVpcs = $.000091 \cdot .01707 \cdot A = .0774 \text{ ft}^3/\text{sec}$

dVpzr = $.000157 \cdot .01978 \cdot B = .0667 \text{ ft}^3/\text{sec}$

dVtot = 3.1588 ft³/sec

RATE of Pzr Press rise =
dVtot * C = 3.1588 * C =

92.91 psi/sec

Equivalent gpm = $(7.48 * 60 * 3.1588 \text{ ft}^3) = 1417.69 \text{ gpm}$

PCS temperature 270° Vf @ 310 psia = .01716 Vf @ 280° & 310 psia = .01725
Pzr temp 410° Vf @ 310 psia = .01978 Vf @ 420° & 310 psia = .01993

dVhpsi = $\frac{1,220 \text{ gpm}}{7.48/60} = 2.7104 \text{ ft}^3/\text{sec}$

dVchg = $\frac{133 \text{ gpm}}{7.48/60} = .2963 \text{ ft}^3/\text{sec}$

dVpcs = $.000091 \cdot .01716 \cdot A = .0770 \text{ ft}^3/\text{sec}$

dVpzr = $.000157 \cdot .01978 \cdot B = .0667 \text{ ft}^3/\text{sec}$

dVtot = 3.1584 ft³/sec

RATE of Pzr Press rise =
dVtot * C = 3.1584 * C =

92.8901 psi/sec

Equivalent gpm = $(7.48 * 60 * 3.1584 \text{ ft}^3) = 1417.4868 \text{ gpm}$

PCS temperature 280° Vf @ 310 psia = .01725 Vf @ 290° & 310 psia = .01734
Pzr temp 410° Vf @ 310 psia = .01978 Vf @ 420° & 310 psia = .01993

dVhpsi = $\frac{1,220 \text{ gpm}}{7.48/60} = 2.7104 \text{ ft}^3/\text{sec}$

dVchg = $\frac{133 \text{ gpm}}{7.48/60} = .2963 \text{ ft}^3/\text{sec}$

dVpcs = $.000091 \cdot .01725 \cdot A = .0766 \text{ ft}^3/\text{sec}$

dVpzr = $.000157 \cdot .01978 \cdot B = .0667 \text{ ft}^3/\text{sec}$

dVtot = 3.1580 ft³/sec

RATE of Pzr Press rise =
dVtot * C = 3.1580 * C =

92.8663 psi/sec

Equivalent gpm = $(7.48 * 60 * 3.1580 \text{ ft}^3) = 1417.3065 \text{ gpm}$

NOTES: 1) BOTH HPSI pumps operable: See page 20 for rates of Pzr Press increase w/o HPSI from 260° to 350°

Constants on this page: A = 14.60 B = 8.3539 C = 29.4131 K = 303,299

23,5188 242,519

PCS temperature 390° Vf @ 310 psia = .01734 Vf' @ 300° & 310 psia = .01743
Pzr temp 410° Vf @ 310 psia = .01879 Vf' @ 420° & 310 psia = .01873

dVhpsi = 1,220 gpm / 7.48 / 60 = 2.7194 ft³/sec

dVchg = 133 gpm / 7.48 / 60 = .2963 ft³/sec

dVpcs = .000091 / .01734 * A = .0762 ft³/sec

RATE of Pzr Press rise =
dVtot * C = 3.1576 * C =

dVpzr = .000151 / .01879 * B = .0667 ft³/sec

92.8746 psi/sec

dVtot = 3.1576 ft³/sec

Equivalent gpm = (7.48 * 60 * 3.1576 ft³) = 1,417.1²⁸¹ gpm

PCS temperature 300° Vf @ 310 psia = .01743 Vf' @ 310° & 310 psia = .01753
Pzr temp 410° Vf @ 310 psia = .01879 Vf' @ 420° & 310 psia = .01893

dVhpsi = 1,220 gpm / 7.48 / 60 = 2.7184 ft³/sec

dVchg = 133 gpm / 7.48 / 60 = .2963 ft³/sec

dVpcs = .000101 / .01743 * A = .0842 ft³/sec

RATE of Pzr Press rise =
dVtot * C = 3.1656 * C =

dVpzr = .000151 / .01879 * B = .0667 ft³/sec

93.110 psi/sec

dVtot = 3.1656 ft³/sec

Equivalent gpm = (7.48 * 60 * 3.1656 ft³) = 1,420.7³¹⁴ gpm

PCS temperature 310° Vf @ 310 psia = .01753 Vf' @ 320° & 310 psia = .01764
Pzr temp 410° Vf @ 310 psia = .01879 Vf' @ 420° & 310 psia = .01893

dVhpsi = 1,220 gpm / 7.48 / 60 = 2.7184 ft³/sec

dVchg = 133 gpm / 7.48 / 60 = .2963 ft³/sec

dVpcs = .000111 / .01753 * A = .0921 ft³/sec

RATE of Pzr Press rise =
dVtot * C = 3.1735 * C =

dVpzr = .000151 / .01879 * B = .0667 ft³/sec

74.6374 psi/sec

dVtot = 3.1735 ft³/sec

Equivalent gpm = (7.48 * 60 * 3.1735 ft³) = 1,424.2⁷⁴¹ gpm

NOTES:

1) C revised as K changed from 303,299 to 242,519

Constants on this page: A = 14.68 B = 8.3539 C = 23.5188 K = 242.519

PCS temperature 320° Vf @ 310 psia = .01764 Vf' @ 320° & 310 psia = .01725
Pzr temp 40° Vf @ 310 psia = .01878 Vf' @ 40° & 310 psia = .01893

$$dV_{hpsi} = \frac{1,220 \text{ gpm}}{7.48/60} = \underline{2.7184} \text{ ft}^3/\text{sec}$$

$$dV_{chg} = \frac{133 \text{ gpm}}{7.48/60} = \underline{.2963} \text{ ft}^3/\text{sec}$$

$$dV_{pcs} = .00011 / (.01764 * A) = \underline{.0915} \text{ ft}^3/\text{sec}$$

$$dV_{pzr} = .00015 / (.01878 * B) = \underline{.0667} \text{ ft}^3/\text{sec}$$

$$dV_{tot} = \underline{3.1729} \text{ ft}^3/\text{sec}$$

$$\text{RATE of Pzr Press rise} = dV_{tot} * C = \underline{3.1729} * C =$$

$$\underline{74.6238} \text{ psi/sec}$$

$$\text{Equivalent gpm} = (7.48 * 60 * \underline{3.1729} \text{ ft}^3) = \underline{1,424.063} \text{ gpm}$$

PCS temperature 330° Vf @ 310 psia = .01775 Vf' @ 330° & 310 psia = .01786
Pzr temp 40° Vf @ 310 psia = .01878 Vf' @ 40° & 310 psia = .01893

$$dV_{hpsi} = \frac{1,220 \text{ gpm}}{7.48/60} = \underline{2.7184} \text{ ft}^3/\text{sec}$$

$$dV_{chg} = \frac{133 \text{ gpm}}{7.48/60} = \underline{.2963} \text{ ft}^3/\text{sec}$$

$$dV_{pcs} = .00011 / (.01775 * A) = \underline{.0910} \text{ ft}^3/\text{sec}$$

$$dV_{pzr} = .00015 / (.01878 * B) = \underline{.0667} \text{ ft}^3/\text{sec}$$

$$dV_{tot} = \underline{3.1724} \text{ ft}^3/\text{sec}$$

$$\text{RATE of Pzr Press rise} = dV_{tot} * C = \underline{3.1724} * C =$$

$$\underline{74.6105} \text{ psi/sec}$$

$$\text{Equivalent gpm} = (7.48 * 60 * \underline{3.1724} \text{ ft}^3) = \underline{1,423.767} \text{ gpm}$$

PCS temperature 340° Vf @ 310 psia = .01786 Vf' @ 340° & 310 psia = .01797
Pzr temp 40° Vf @ 310 psia = .01878 Vf' @ 40° & 310 psia = .01893

$$dV_{hpsi} = \frac{1,220 \text{ gpm}}{7.48/60} = \underline{2.7184} \text{ ft}^3/\text{sec}$$

$$dV_{chg} = \frac{133 \text{ gpm}}{7.48/60} = \underline{.2963} \text{ ft}^3/\text{sec}$$

$$dV_{pcs} = .00011 / (.01786 * A) = \underline{.0904} \text{ ft}^3/\text{sec}$$

$$dV_{pzr} = .00015 / (.01878 * B) = \underline{.0667} \text{ ft}^3/\text{sec}$$

$$dV_{tot} = \underline{3.1718} \text{ ft}^3/\text{sec}$$

$$\text{RATE of Pzr Press rise} = dV_{tot} * C = \underline{3.1718} * C =$$

$$\underline{74.5973} \text{ psi/sec}$$

$$\text{Equivalent gpm} = (7.48 * 60 * \underline{3.1718} \text{ ft}^3) = \underline{1,423.5103} \text{ gpm}$$

NOTES:

Constants on this page: A = 24,467 B = 0.3539 C = 23.5188 K = 242.519 1)

PCS temperature 350° Vf @ 700 psia = .01794 Vf' @ 360° & 700 psia = .01806
Pzr temp 490° Vf @ 700 psia = .02020 Vf' @ 520° & 700 psia = .02093

2) $dV_{hpsi} = \frac{950 \text{ gpm}}{7.48/60} = 2.1168 \text{ ft}^3/\text{sec}$

$dV_{chg} = \frac{133 \text{ gpm}}{7.48/60} = .2963 \text{ ft}^3/\text{sec}$

1) $dV_{pcs} = .00012 / .01794 * A = .1637 \text{ ft}^3/\text{sec}$

RATE of Pzr Press rise =
 $dV_{tot} * C = 2.6719 * C =$

1) $dV_{pzr} = .00023 / .02020 * B = .095 \text{ ft}^3/\text{sec}$

62.8404 psi/sec

$dV_{tot} = 2.6719 \text{ ft}^3/\text{sec}$

Equivalent gpm = $(7.48 * 60 * 2.6719 \text{ ft}^3) = 1,192.1571 \text{ gpm}$

PCS temperature 360° Vf @ 900 psia = .01804 Vf' @ 370° & 900 psia = .01816
Pzr temp 520° Vf @ 900 psia = .02089 Vf' @ 530° & 900 psia = .02117

$dV_{hosi} = \frac{720 \text{ gpm}}{7.48/60} = 1.728 \text{ ft}^3/\text{sec}$

$dV_{chg} = \frac{133 \text{ gpm}}{7.48/60} = .2963 \text{ ft}^3/\text{sec}$

$dV_{pcs} = .00012 / .01804 * A = .1627 \text{ ft}^3/\text{sec}$

RATE of Pzr Press rise =
 $dV_{tot} * C = 2.3090 * C =$

$dV_{pzr} = .00020 / .02089 * B = .1120 \text{ ft}^3/\text{sec}$

54.3043 psi/sec

$dV_{tot} = 2.3090 \text{ ft}^3/\text{sec}$

Equivalent gpm = $(7.48 * 60 * 2.3090 \text{ ft}^3) = 1,036.266 \text{ gpm}$

PCS temperature 370° Vf @ 1,100 psia = .01814 Vf' @ 380° & 1,100 psia = .01827
Pzr temp 540° Vf @ 1,100 psia = .02141 Vf' @ 550° & 1,100 psia = .02173

$dV_{hpsi} = \frac{550 \text{ gpm}}{7.48/60} = 1.2255 \text{ ft}^3/\text{sec}$

$dV_{chg} = \frac{133 \text{ gpm}}{7.48/60} = .2963 \text{ ft}^3/\text{sec}$

$dV_{pcs} = .00013 / .01814 * A = .1753 \text{ ft}^3/\text{sec}$

RATE of Pzr Press rise =
 $dV_{tot} * C = 1.822 * C =$

$dV_{pzr} = .00032 / .02141 * B = .1249 \text{ ft}^3/\text{sec}$

42.8513 psi/sec

$dV_{tot} = 1.822 \text{ ft}^3/\text{sec}$

Equivalent gpm = $(7.48 * 60 * 1.822 \text{ ft}^3) = 817.7136 \text{ gpm}$

- NOTES: 1) Begin heating PCS @ 100°/hr, and increase Pzr Press from 310 psia to 700 psia
2) HPSI must be operable at this temp. & above.

Constants on this page: A = 24.4667 B = 0.3539 C = 23.5188 K = 242,519

17.0722 176,043

PCS temperature 380° Vf @ 1,200psia = .01826 Vf @ 380° & 1,200psia = .01839
Pzr temp 550° Vf @ 1,200psia = .02170 Vf @ 550° & 1,200psia = .02205

$$dV_{hpsi} = 350 \text{ gpm} / 7.48 / 60 = .7799 \text{ ft}^3/\text{sec}$$

$$dV_{chg} = 133 \text{ gpm} / 7.48 / 60 = .2963 \text{ ft}^3/\text{sec}$$

$$dV_{pcs} = .00013 / .01826 * A = .1742 \text{ ft}^3/\text{sec}$$

$$\text{RATE of Pzr Press rise} = dV_{tot} * C = 1.305 / * C =$$

$$dV_{pzr} = .000357 / .02170 * B = .1347 \text{ ft}^3/\text{sec}$$

$$32.5769 \text{ psi/sec}$$

$$dV_{tot} = 1.305 / \text{ft}^3/\text{sec}$$

$$\text{Equivalent gpm} = (7.48 * 60 * 1.305 / \text{ft}^3) = 621.6510 \text{ gpm}$$

PCS temperature 370° Vf @ 1,400psia = .01837 Vf @ 370° & 1,400psia = .01850
Pzr temp 570° Vf @ 1,400psia = .02234 Vf @ 570° & 1,400psia = .02275

$$1) dV_{hpsi} = 0 \text{ gpm} / 7.48 / 60 = \text{---} \text{ ft}^3/\text{sec}$$

$$dV_{chg} = 133 \text{ gpm} / 7.48 / 60 = .2963 \text{ ft}^3/\text{sec}$$

$$dV_{pcs} = .00013 / .01837 * A = .1731 \text{ ft}^3/\text{sec}$$

$$\text{RATE of Pzr Press rise} = dV_{tot} * C = .6227 * C =$$

$$dV_{pzr} = .00041 / .02234 * B = .1533 \text{ ft}^3/\text{sec}$$

$$14.6456 \text{ psi/sec}$$

$$dV_{tot} = .6227 \text{ ft}^3/\text{sec}$$

$$\text{Equivalent gpm} = (7.48 * 60 * .6227 \text{ ft}^3) = 279.453 \text{ gpm}$$

PCS temperature 400° Vf @ 1,500psia = .01849 Vf @ 400° & 1,500psia = .01863
Pzr temp 580° Vf @ 1,500psia = .02270 Vf @ 580° & 1,500psia = .02315

$$dV_{hpsi} = 0 \text{ gpm} / 7.48 / 60 = \text{---} \text{ ft}^3/\text{sec}$$

$$dV_{chg} = 133 \text{ gpm} / 7.48 / 60 = .2963 \text{ ft}^3/\text{sec}$$

$$dV_{pcs} = .00014 / .01849 * A = .1853 \text{ ft}^3/\text{sec}$$

$$\text{RATE of Pzr Press rise} = dV_{tot} * C = .6472 * C =$$

$$dV_{pzr} = .00045 / .02270 * B = .1656 \text{ ft}^3/\text{sec}$$

$$11.0492 \text{ psi/sec}$$

$$dV_{tot} = .6472 \text{ ft}^3/\text{sec}$$

$$\text{Equivalent gpm} = (7.48 * 60 * .6472 \text{ ft}^3) = 290.466 \text{ gpm}$$

- NOTES:
- 1) Pzr Press > HPSI Shutoff head ... no further contribution from HPSI
 - 2) C revised as K changed from 242,519 to 176,043

Constants on this page: A = 24.4667 B = 8.3539 C = 17.0722 K = 176,043

PCS temperature 40° Vf @ 1,500psia = .01863 Vf @ 420° & 1,500psia = .01878
Pzr temp 580° Vf @ 1,500psia = .02270 Vf @ 590° & 1,500psia = .02315

$$dV_{hpsi} = \underline{0} \text{ gpm}/7.48/60 = \underline{\quad\quad\quad} \text{ft}^3/\text{sec}$$

$$dV_{chg} = 133 \text{ gpm}/7.48/60 = .2963 \text{ ft}^3/\text{sec}$$

$$dV_{pcs} = .00015 / .01863 * A = .1970 \text{ ft}^3/\text{sec}$$

$$\text{RATE of Pzr Press rise} = dV_{tot} * C = \underline{.6589} * C =$$

$$dV_{pzr} = .000457 / .02270 * B = .1656 \text{ ft}^3/\text{sec}$$

$$\underline{11.2487} \text{ psi/sec}$$

$$dV_{tot} = \underline{.6589} \text{ ft}^3/\text{sec}$$

$$\text{Equivalent gpm} = (7.48 * 60 * \underline{.6589} \text{ ft}^3) = \underline{295.7117} \text{ gpm}$$

PCS temperature 420° Vf @ 1,600psia = .01877 Vf @ 430° & 1,600psia = .01892
Pzr temp 590° Vf @ 1,600psia = .02309 Vf @ 600° & 1,600psia = .02359

$$dV_{hpsi} = \underline{0} \text{ gpm}/7.48/60 = \underline{\quad\quad\quad} \text{ft}^3/\text{sec}$$

$$dV_{chg} = 133 \text{ gpm}/7.48/60 = .2963 \text{ ft}^3/\text{sec}$$

$$dV_{pcs} = .00015 / .01877 * A = .1955 \text{ ft}^3/\text{sec}$$

$$\text{RATE of Pzr Press rise} = dV_{tot} * C = \underline{.6727} * C =$$

$$dV_{pzr} = .00050 / .02309 * B = .1809 \text{ ft}^3/\text{sec}$$

$$\underline{11.4849} \text{ psi/sec}$$

$$dV_{tot} = \underline{.6727} \text{ ft}^3/\text{sec}$$

$$\text{Equivalent gpm} = (7.48 * 60 * \underline{.6727} \text{ ft}^3) = \underline{301.9189} \text{ gpm}$$

PCS temperature 430° Vf @ 1,800psia = .01890 Vf @ 440° & 1,800psia = .01905
Pzr temp 610° Vf @ 1,800psia = .02400 Vf @ 620° & 1,800psia = .02465

$$dV_{hpsi} = \underline{0} \text{ gpm}/7.48/60 = \underline{\quad\quad\quad} \text{ft}^3/\text{sec}$$

$$dV_{chg} = 133 \text{ gpm}/7.48/60 = .2963 \text{ ft}^3/\text{sec}$$

$$dV_{pcs} = .00015 / .01890 * A = .1942 \text{ ft}^3/\text{sec}$$

$$\text{RATE of Pzr Press rise} = dV_{tot} * C = \underline{.7168} * C =$$

$$dV_{pzr} = .00065 / .02400 * B = .2263 \text{ ft}^3/\text{sec}$$

$$\underline{12.2370} \text{ psi/sec}$$

$$dV_{tot} = \underline{.7168} \text{ ft}^3/\text{sec}$$

$$\text{Equivalent gpm} = (7.48 * 60 * \underline{.7168} \text{ ft}^3) = \underline{321.6908} \text{ gpm}$$

NOTES:

Constants on page A = 24.4667 B = 8.3539 C = 17.072 K = 176,043

PCS temperature 740° Vf @ 1800psia = .01905 Vf @ 450° & 1800psia = .01922
Pzr temp 610° Vf @ 1800psia = .02400 Vf @ 620° & 1800psia = .02465

dVhpsi = 0 gpm/7.48/60 = _____ ft3/sec

dVchg = 133gpm/7.48/60 = .2963ft3/sec

dVpcs = .0007/.01905*A = .2183 ft3/sec

RATE of Pzr Press rise =
dVtot*C = .7409*C =

dVpzr = .000657/.02400*B = .2263 ft3/sec

12.6494 psi/sec

dVtot = .7409 ft3/sec

Equivalent gpm = (7.48*60* .7409 ft3) = 332.533 gpm

PCS temperature 450° Vf @ 1800psia = .01922 Vf @ 460° & 1800psia = .01939
Pzr temp 610° Vf @ 1800psia = .02400 Vf @ 620° & 1800psia = .02465

dVhpsi = 0 gpm/7.48/60 = _____ ft3/sec

dVchg = 133gpm/7.48/60 = .2963ft3/sec

dVpcs = .0007/.01922*A = .2164 ft3/sec

RATE of Pzr Press rise =
dVtot*C = .7390*C =

dVpzr = .000657/.02400*B = .2263 ft3/sec

12.6165 psi/sec

dVtot = .7390 ft3/sec

Equivalent gpm = (7.48*60* .7390 ft3) = 331.663 gpm

PCS temperature ___ Vf @ ___ psia = ___ Vf @ ___ & ___ psia = ___
Pzr temp ___ Vf @ ___ psia = ___ Vf @ ___ & ___ psia = ___

dVhpsi = ___ gpm/7.48/60 = _____ ft3/sec

dVchg = 133gpm/7.48/60 = .2963ft3/sec

dVpcs = .000 / .01 *A = _____ ft3/sec

RATE of Pzr Press rise =
dVtot*C = _____ *C =

dVpzr = .000 / .0 *B = _____ ft3/sec

_____ psi/sec

dVtot = _____ ft3/sec

Equivalent gpm = (7.48*60* _____ ft3) = _____ gpm

NOTES:

Constants on this page: A = 14.68 B = 0.3539 C = 29.4131 K = 303,299

Following APPLICABLE WITH NO HPSI PUMPS OPERABLE 1)

PCS temperature 260° Vf @ 310 psia = .01707 Vf @ 270° & 310 psia = .01716
Pzr temp 410° Vf @ 310 psia = .01878 Vf @ 420° & 310 psia = .01893

$$dV_{hpsi} = \frac{N/A}{7.48/60} \text{ gpm} = \text{ft}^3/\text{sec}$$

$$dV_{chg} = 133 \text{ gpm} / 7.48/60 = .2963 \text{ ft}^3/\text{sec}$$

$$dV_{pcs} = .00009 / .01707 * A = .0774 \text{ ft}^3/\text{sec}$$

$$\text{RATE of Pzr Press rise} = dV_{tot} * C = .4404 * C =$$

$$dV_{pzr} = .00015 / .01878 * B = .0667 \text{ ft}^3/\text{sec}$$

$$12.9535 \text{ psi/sec}$$

$$dV_{tot} = .4404 \text{ ft}^3/\text{sec}$$

$$\text{Equivalent gpm} = (7.48 * 60 * .4404 \text{ ft}^3) = 197.6515 \text{ gpm}$$

PCS temperature 270° Vf @ 310 psia = .01716 Vf @ 280° & 310 psia = .01725
Pzr temp 410° Vf @ 310 psia = .01878 Vf @ 420° & 310 psia = .01893

$$dV_{hpsi} = \frac{N/A}{7.48/60} \text{ gpm} = \text{ft}^3/\text{sec}$$

$$dV_{chg} = 133 \text{ gpm} / 7.48/60 = .2963 \text{ ft}^3/\text{sec}$$

$$dV_{pcs} = .00009 / .01716 * A = .0770 \text{ ft}^3/\text{sec}$$

$$\text{RATE of Pzr Press rise} = dV_{tot} * C = .4400 * C =$$

$$dV_{pzr} = .00015 / .01878 * B = .0667 \text{ ft}^3/\text{sec}$$

$$12.9418 \text{ psi/sec}$$

$$dV_{tot} = .4400 \text{ ft}^3/\text{sec}$$

$$\text{Equivalent gpm} = (7.48 * 60 * .4400 \text{ ft}^3) = 197.472 \text{ gpm}$$

PCS temperature 280° Vf @ 310 psia = .01725 Vf @ 290° & 310 psia = .01734
Pzr temp 410° Vf @ 310 psia = .01878 Vf @ 420° & 310 psia = .01893

$$dV_{hpsi} = \frac{N/A}{7.48/60} \text{ gpm} = \text{ft}^3/\text{sec}$$

$$dV_{chg} = 133 \text{ gpm} / 7.48/60 = .2963 \text{ ft}^3/\text{sec}$$

$$dV_{pcs} = .00009 / .01725 * A = .0766 \text{ ft}^3/\text{sec}$$

$$\text{RATE of Pzr Press rise} = dV_{tot} * C = .4396 * C =$$

$$dV_{pzr} = .00015 / .01878 * B = .0667 \text{ ft}^3/\text{sec}$$

$$12.93 \text{ psi/sec}$$

$$dV_{tot} = .4396 \text{ ft}^3/\text{sec}$$

$$\text{Equivalent gpm} = (7.48 * 60 * .4396 \text{ ft}^3) = 197.2725 \text{ gpm}$$

NOTES: 1) See page 13 for rates of Pzr Press Increase w/ HPSI

Constants on this page: A = 14.68 B = 0.3539 C = 29.4131 K = 303,299

23.5188 242,519

PCS temperature 290° Vf @ 310 psia = .01734 Vf @ 300 & 310 psia = .01743
Pzr temp 410° Vf @ 310 psia = .01878 Vf @ 420 & 310 psia = .01853

dVhpsi = $\frac{N/A \text{ gpm}}{7.48/60} = \text{ft}^3/\text{sec}$

dVchg = $\frac{133 \text{ gpm}}{7.48/60} = .2963 \text{ ft}^3/\text{sec}$

RATE of Pzr Press rise =
dVtot * C = .4392 * C =

dVpcs = $.00009 / .01734 * A = .0762 \text{ ft}^3/\text{sec}$

12.9182 psi/sec

dVpzr = $.000157 / .01878 * B = .0667 \text{ ft}^3/\text{sec}$

dVtot = .4392 ft³/sec

Equivalent gpm = (7.48 * 60 * .4392 ft³) = 197.113 gpm

PCS temperature 300° Vf @ 310 psia = .01743 Vf @ 310 & 310 psia = .01753
Pzr temp 410° Vf @ 310 psia = .01878 Vf @ 420 & 310 psia = .01853

dVhpsi = $\frac{N/A \text{ gpm}}{7.48/60} = \text{ft}^3/\text{sec}$

dVchg = $\frac{133 \text{ gpm}}{7.48/60} = .2963 \text{ ft}^3/\text{sec}$

RATE of Pzr Press rise =
dVtot * C = .4472 * C =

dVpcs = $.00010 / .01743 * A = .0842 \text{ ft}^3/\text{sec}$

13.1535 psi/sec

dVpzr = $.000151 / .01878 * B = .0667 \text{ ft}^3/\text{sec}$

dVtot = .4472 ft³/sec

Equivalent gpm = (7.48 * 60 * .4472 ft³) = 200.7034 gpm

PCS temperature 310° Vf @ 310 psia = .01753 Vf @ 320 & 310 psia = .01764
Pzr temp 410° Vf @ 310 psia = .01878 Vf @ 420 & 310 psia = .01853

dVhpsi = $\frac{N/A \text{ gpm}}{7.48/60} = \text{ft}^3/\text{sec}$

dVchg = $\frac{133 \text{ gpm}}{7.48/60} = .2963 \text{ ft}^3/\text{sec}$

RATE of Pzr Press rise =
dVtot * C = .4551 * C =

dVpcs = $.00011 / .01753 * A = .0921 \text{ ft}^3/\text{sec}$

10.7034 psi/sec

dVpzr = $.000151 / .01878 * B = .0667 \text{ ft}^3/\text{sec}$

dVtot = .4551 ft³/sec

Equivalent gpm = (7.48 * 60 * .4551 ft³) = 204.2489 gpm

NOTES: 1) C revised as K changed from 303,299 to 242,519

Constants on this page: A = 14.68 B = 8.3539 C = 23.5188 K = 242.519

PCS temperature 320° Vf @ 310 psia = .01764 Vf @ 330° & 310 psia = .01775
 Fzr temp 410° Vf @ 310 psia = .01878 Vf @ 420° & 310 psia = .01893

dVhpsi = N/A gpm/7.48/60 = _____ ft³/sec

dVchg = 133gpm/7.48/60 = .2963ft³/sec

dVpcs = .00011 / .01764 * A = .0915 ft³/sec

RATE of Fzr Press rise =
dVtot * C = .4545 * C =

dVpzr = .00015 / .01878 * B = .0667 ft³/sec

10.6893 psi/sec

dVtot = .4545 ft³/sec

Equivalent gpm = (7.48*60* .4545 ft³) = 203.9796 gpm

PCS temperature 330° Vf @ 310 psia = .01775 Vf @ 340° & 310 psia = .01786
 Fzr temp 410° Vf @ 310 psia = .01878 Vf @ 420° & 310 psia = .01893

dVhpsi = N/A gpm/7.48/60 = _____ ft³/sec

dVchg = 133gpm/7.48/60 = .2963ft³/sec

dVpcs = .00011 / .01775 * A = .0910 ft³/sec

RATE of Fzr Press rise =
dVtot * C = .4540 * C =

dVpzr = .00015 / .01878 * B = .0667 ft³/sec

10.6775 psi/sec

dVtot = .4540 ft³/sec

Equivalent gpm = (7.48*60* .4540 ft³) = 203.7552 gpm

PCS temperature 340° Vf @ 310 psia = .01786 Vf @ 350° & 310 psia = .01797
 Fzr temp 410° Vf @ 310 psia = .01878 Vf @ 420° & 310 psia = .01893

dVhpsi = N/A gpm/7.48/60 = _____ ft³/sec

dVchg = 133gpm/7.48/60 = .2963ft³/sec

dVpcs = .00011 / .01786 * A = .0908 ft³/sec

RATE of Fzr Press rise =
dVtot * C = .4534 * C =

dVpzr = .00015 / .01878 * B = .0667 ft³/sec

10.6634 psi/sec

dVtot = .4534 ft³/sec

Equivalent gpm = (7.48*60* .4534 ft³) = 203.4859 gpm

NOTES:

1) From 350° and above, HPSI pumps are operable.

Conclusions:

Pressurizer pressure rate of change is defined for the assumptions taken.

References:

- 1) FLUID MECHANICS, Daugherty and Franzini, 7th edition, c. 1977
- 2) ANF-88-107, Palisades LOCA-ECCS Analysis for 2530 Mwt Operation with Increased Radial Peaking and 29.3% Steam Generator Tube Plugging
- 3) Palisades Plant Functional Description M10, Primary Coolant System, rev 1
- 4) Palisades Plant Technical Specifications Change Request, 1989, affecting HPSI Operability Requirements, and PCS Heating and Cooling Rates
- 5) ASME Steam Tables, 4th edition, c. 1979
- 6) Letter to DJVandewalle, CPCo, from WDMeinert, CE, 1 Jan 79, P-CE-4538; Attachment 1, HPI SYSTEM DELIVERY - ONE HPI PUMP THROUGH FOUR HPI VALVES

Title PRESSURE RESPONSE EFFECTS OF VLTOP WITH REPLACEMENT PORVS.

INITIATION AND REVIEW

Rev #	Description	Initiated		Initiator Appd By	Review Method Check (✓)			Technically Reviewed		Reviewer Appd By
		By	Date		Alt Calc	Det Rvw	Qual Test	By	Date	
0	Original Issue									

CALCULATE THE BULK MODULUS OF ELASTICITY FOR WATER AT 10° INTERVALS FROM 50° F TO 200° F, AND AT 50° C INTERVALS FROM 200° F TO 450° F.

FOR TEMPERATURES FROM 50° F TO 200° F, VALUES ARE INTERPOLATED FROM TABLE 1.1 OF REFERENCE 1. FOR TEMPERATURES FROM 200° F TO 450° F, VALUES ARE CALCULATED FROM DATA IN TABLE C.2 OF REFERENCE 5.

TABLE 1.1 HAS VALUES FOR 32°, 68°, 120°, AND 200°, SO INTERPOLATION IS NECESSARY FOR 10° INCREMENTAL VALUES. ALSO, TABLE 1.1 HAS VALUES FOR 15 psia, AND 1500 psia, SO ANOTHER INTERPOLATION IS REQUIRED FOR 310 psia. THE TWO INTERPOLATED VALUES MUST IN TURN BE INTERPOLATED TO ARRIVE AT VALUE FOR TEMPERATURE AND PRESSURE OF INTEREST.

310 psia REPRESENTS .1987 OF THE RANGE FROM 15 psia TO 1500 psia
 $(310 - 15) / (1500 - 15) = .1987$

FINAL INTERPOLATED VALUES ARE DERIVED FROM TABLE 1.1 AS FOLLOWS:

- a) INTERPOLATE FOR DESIRED TEMP @ 15 psia
- b) " " " " @ 1500 psia
- c) " " 310 psia @ Desired Temp.



PALISADES NUCLEAR PLANT
ANALYSIS CONTINUATION SHEET

ATTACHMENT 1 TO
EA-PC-809-13 Rev 1
Sheet 2 of 2
Rev #

PCS	K@	K@	K@	K@	K@	K@	K@	Reference Comments
TEMP	32°/15 psi	68°/15 psi	*/15 psi	32°/1500	68°/1500	*/1500	*/310 psi	Rev 1
*								
50	292,000	320,000	306,000	300,000	330,000	315,000	307,788	
60	292,000	320,000	313,778	300,000	330,000	323,333	315,675	
	68°/15 psi	120°/15 psi		68°/1500	120°/1500			
70	320,000	332,000	320,462	330,000	342,000	330,462	322,449	
80	320,000	332,000	322,769			332,769	324,756	
90			325,077			335,077	327,064	
100			327,385			337,385	329,372	
110			329,692			339,692	331,679	
120			332,000			342,000	333,987	
	120°/15 psi	200°/15 psi		120°/1500	200°/1500			
130	332,000	308,000	329,000	342,000	319,000	339,125	331,012	
140			326,000			336,250	328,037	
150			323,000			333,375	325,062	
160			320,000			330,500	322,086	
170			317,000			327,625	319,111	
180			314,000			324,750	316,136	
190			311,000			321,875	313,161	
200			308,000			319,000	310,186	

CALCULATING K from ref 5 table C.2 data, $K =$

$$P_1 - P_2 / ((V_1 - V_2) / V_1) * (1 \text{ atmosphere in psi})$$

where P_1 and P_2 are in atmospheres, and V_1 and V_2 are specific volumes of water at the respective pressures.

From reference 5, conversion factor from bar to psi =

$$14.5037738$$

$$\text{@ } 100^\circ\text{C, } K = (25 - 225) / ((1.04245 - 1.03248) / 1.04245) * 14.5037738 = -303,299$$

$$\text{@ } 150^\circ\text{C, } K = -200 / ((1.08938 - 1.07635) / 1.08938) * 14.5037738 = 242,519$$

$$\text{@ } 200^\circ\text{C, } K = -200 / ((1.15551 - 1.13647) / 1.15551) * 14.5037738 = 176,043$$

$$\text{@ } 250^\circ\text{C, } K = -200 / ((1.24941 - 1.21751) / 1.24941) * 14.5037738 = 113,612$$

ENGINEERING ANALYSIS

Title: Pressure Response Effects of VLTOP with Replacement PORVs
Part II - PORV FLOW versus TIME for NEW PORVs (Target Rock)

Objective:

Determine the water flow after reaching full stroke position for the new PORVs, as input to calculate pressurizer pressure overshoot during LTOP actuation.

Analysis Input:

- a) PORV Cv = 219 at full stroke (ref 1)
- b) PORV main disc slew (stroke) time = 0.20 seconds (ref 5)
- c) PORV solenoid and pilot chamber reaction time = 1.68 seconds (ref 5)
- d) Instrument channel reaction time = .2 seconds (ref 3)
- e) PORV full stroke effective area = 5.7732 square inches (ref 2)
- f) PORV lift and effective area versus time from reference 5.
- g) PORV flow = $Cv \cdot \sqrt{dP}$

Assumptions:

- a) Available dP = Pressurizer pressure - Quench Tank pressure
- b) Quench Tank pressure = 100 psig (90 psig RuD setting +10 psi margin)
- c) PORV stroke time will lessen with increasing subcooling; ie, longest response time (1.68 seconds) with associated stroke time (0.20 seconds) from the computer model will envelope times with lower pressurizer temperatures. That is, time for full valve stroke will be less with sufficient subcooling of the fluid in the PORV control chamber.

Calculations:

Begin of page following

PORV FLOW versus TIME
(From Reference 5)

1)	2)	3)	4)	5)	6)	7)	8)
Graph Time	Lift mils	Effect. Area	Effect. Area / F.S.Eft Ar.	Cv (219*4)	Sqrt dP @310 s.p	Sqrt dP @700 s.p	Sqrt dP @900 s.p
9)	10)	Flow = Cv * Sqrt dP			11)	12)	13)
Adjusted Time	Total Time	= 5) * 6)			Flow @ 310 sp	Flow @ 700 sp	Flow @ 900 sp
		= 5) * 7)					
		= 5) * 8)					

1)	2)	3)	4)	5)	6)	7)	8)
Graph Time	Lift mils	Effect. Area	Effect. Area / F.S.Eft Ar.	Cv (219*4)	Sqrt dP @310 s.p	Sqrt dP @700 s.p	Sqrt dP @900 s.p
9)	10)	Flow = Cv * Sqrt dP			11)	12)	13)
Adjusted Time	Total Time	= 5) * 6)			Flow @ 310 sp	Flow @ 700 sp	Flow @ 900 sp
		= 5) * 7)					
		= 5) * 8)					

1)	2)	3)	4)	5)	6)	7)	8)
Graph Time	Lift mils	Effect. Area	Effect. Area / F.S.Eft Ar.	Cv (219*4)	Sqrt dP @310 s.p	Sqrt dP @700 s.p	Sqrt dP @900 s.p
9)	10)	Flow = Cv * Sqrt dP			11)	12)	13)
Adjusted Time	Total Time	= 5) * 6)			Flow @ 310 sp	Flow @ 700 sp	Flow @ 900 sp
		= 5) * 7)					
		= 5) * 8)					

1)	2)	3)	4)	5)	6)	7)	8)
Graph Time	Lift mils	Effect. Area	Effect. Area / F.S.Eft Ar.	Cv (219*4)	Sqrt dP @310 s.p	Sqrt dP @700 s.p	Sqrt dP @900 s.p
N/A	1,000	5.7732	1.0	219	13.96		
9)	10)	Flow = Cv * Sqrt dP			11)	12)	13)
Adjusted Time	Total Time	= 5) * 6)			Flow @ 310 sp	Flow @ 700 sp	Flow @ 900 sp
1,880	<u>2,080</u>	= 5) * 7)			3,057		
		= 5) * 8)			GPM		

PORV FLOW versus TIME

RESULTS

TIME msec	STROKE mils	EFFECTIVE AREA (interp sq in)	Cv (Area)	VdP (from Pzr @ 310	flow (gpm)	VdP (Pzr @ 700	flow (gpm)	VdP (Pzr @ 900	flow (gpm)
2,080	1,000	5.7732	219	13.96	3,057	<----not evaluated---->			

2,080 1,000 5.7732 219 13.96 3,057 <----not evaluated---->

(ONLY FULL VALVE STROKE CONSIDERED IN THIS REVISION)

Conclusions:

The expected PORV flow versus dP identified above is conservatively calculated due to the assumptions made.

References:

- 1) Target Rock Test Data, Fascimile Transmitted 11 July 1989, 1345
- 2) Target Rock Test Data, Fascimile Transmitted 26 July 1989, 1453
- 3) Combustion Engineering Proposal for Variable Set Point LTOP, Proposal #88-240-AIA, Section II.4, page 6
- 4) Palisades Instrument Index, M-311, sheet 01-31
- 5) Letter, L. E. Demick, MPR Asc. Inc, to J. L. Topper, CPCo, 12 September 1989, #98-108-07, COMPUTED STROKE TIMES for PALISADES REPLACEMENT
- 6) Letter, L. E. Demick, MPR Asc. Inc, to J. L. Topper, CPCo, 18 September 1989, #98-108-09, VALIDATION of DYNAMIC MODELING APPROACH and PROGRAM for the REPLACEMENT PORVs at PALISADES NUCLEAR POWER PLANT.

MPR ASSOCIATES, INC.

September 12, 1989
98-108-07

Mr. James L. Topper
Consumers Power Company
1945 West Parnall Road
Jackson, MI 49201

Subject: Computed Stroke Times for Palisades Replacement Power Operated Relief Valves

Reference: GWO 8304, File -011, -317.0

Dear Mr. Topper:

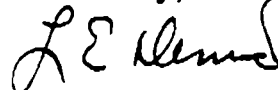
In accordance with our telephone conversation of September 12, 1989 and my subsequent discussion with Mr. Ashworth of CPCo, we have computed the expected opening stroke times for the Palisades replacement Target Rock Power Operated Relief Valves (PORV) for several LTOP set points assuming saturation conditions in the pressurizer. These computations included the effects of the RCS pressure ramp rates that have been calculated by CPCo personnel at these LTOP set points. The following summarizes the results of the computations and identifies the conditions analyzed.

Pressure Set Point (psia)	Pressurizer Temp (°F)	Ramp Rate (psi/sec)	Coil Energize Time (sec)	Depressurize Time (sec)	Slew Time (sec)	Total Time (sec)
330.0	426.1	93.0	0.23	1.45	0.20	1.88
500.0	467.1	93.0	0.26	1.41	0.16	1.83
1000.0	544.6	63.0	0.32	0.97	0.10	1.39

These analyses assume no subcooling in the fluid at the LTOP set point and, therefore, represent an upper limit on the temperature conditions of the pressurizer when the setpoint pressure is reached. We consider this assumption to be very conservative yet the analyses indicate that the valve will open within 2 seconds. As indicated in prior analyses any subcooling of the fluid will reduce the total valve response time.

This information will be included in the final report. If you have any questions or require further information please give me a call.

Sincerely,



L. E. Demick

MPR ASSOCIATES, INC.

September 18, 1989
98-108-09

Mr. James L. Topper
Consumers Power Company
1945 West Parnall Road
Jackson, MI 49201

Subject: Validation of Dynamic Modeling Approach and Program for the
Replacement Power Operated Relief Valves at Palisades Nuclear
Power Plant

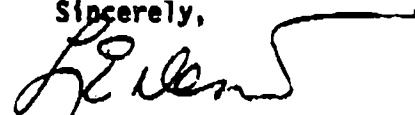
Reference: GWO 8304, File -011, -317.0

In accordance with our telephone conversation of September 18, 1989, the purpose of this letter is to confirm our confidence in the accuracy and validity of the computer program and the approach, which have been used to calculate the opening and closing times for the replacement PORV's to be installed in Palisades this fall. This confidence is based in part on the results of calculations of the stroke times of similar valves in tests performed by EPRI at Wyle facilities in Norco, California. These calculations, reported in a letter to CPCo dated September 15, 1989 (98-108-08), showed good correlation with the test data. Variations between the calculated and test data were also generally in the conservative direction, e.g., calculated opening times for the water tests were generally slower than the test data.

We have also calculated the response of the Palisades replacement valves over a wide range of fluid conditions and consider the variations to be consistent with expectations for this valve design, e.g., more rapid response for steam conditions than for sub-cooled water and more delayed response for saturated water conditions. These data were reported to CPCo in letters dated September 7, 1989 (98-108-06) and September 12, 1989 (98-108-07).

We intend to include complete documentation of the validation basis for the computer program and the valve models in our final report on the replacement valve stroke time analyses. In the meantime if you have any questions concerning these matters or require further information, please give me a call.

Sincerely,



L. E. Demick

ENGINEERING ANALYSIS

Title: Pressure Response Effects of VLTOP with Replacement PORVs
Part III - Recommended LTOP Set Points for Variable LTOP Protection

Objective:

Determine the LTOP set points to preclude exceeding Appx. G Limits, considering :

- . Permissible heating/cooling rates
- . Signal processing time
- . PORV response time
- . Instrument inaccuracies, calibration errors, and drift
- . Potential Quench Tank backpressure

Analysis Inputs:

- a) Pressurizer temperature rate of change is 200 degrees F/hr
- b) Primary Coolant System temperature rate of change is:
 - 20 deg/hr when < 170 degrees F
 - 40 deg/hr when 170 to 250 degrees F
 - 60 deg/hr when 250 to 350 degrees F
 - 100 deg/hr when 350 degrees F and greater
- c) Appendix G limits from EA-A-PAL-89-98
- d) Instrument inaccuracies, calibration errors, and drift are less than 5 degrees and 30 psi (reference 5)
- e) Volume change, equivalent gpm, Bulk Modulus of Elasticity, and pressure increase rates from Part I of this analysis
- f) Time for PORV flow to equal equivalent gpm from Part II of this analysis
- g) Appendix G Limit Equations from reference 4

Assumptions:

- a) Signal Processing Delay is 200 milliseconds (reference 3)
 - b) PORV response time is 1680 milliseconds (reference 6)
 - c) PORV full stroke opening time is 200 milliseconds (reference 6)
 - d) PORV Cv at partial stroke is proportional to effective area
 - e) Quench Tank pressure will not exceed 100 psig
- HPSI pumps are inoperable when shutdown cooling is onstream
- g) HPSI pumps are inoperable when PCS is < 260 deg F

Calculations:

Equation 1, Heating Limited

$$Plim = (17.206 \times (26.78 + (1.233 \times \text{Exp}(.0145 \times (T - 86 - dT1/4)))) - 84$$

Equation 2, Cooling Limited

$$Plim = (17.206 \times (26.78 + (1.233 \times \text{Exp}(.0145 \times (T - 86 + dT1/4)))) - (5.85 \times dTmax) - 84$$

Where Plim = Recommended set point in PSIG before allowance for overshoot,

T = PCS temperature, degrees F

dT1/4 for	Heating	Cooling	dTmax for Cooling
20deg/hr	6.3	4.4	10.1
40deg/hr	12.4	9.0	20.5
60deg/hr	18.2	13.9	31.8
100deg/hr	30.0	23.6	54.0

←---from Part I---							---> <Part II>(7x8)		PSIG	PSIA
1	2	3	4	5	6	7	8	9	10	11
PCS Temp degF	Htg/Clg Rate deg/hr	Pumps Operable	dV/sec Cu.ft	Equip gpm	K	Rate of Press Increase psi/sec	Time for PORV flo:O'sht in sec's	Press =Equivalent psi	Appx G Limit -Temp& Press	Max Perm Set Pnt Errors
50	20	3 Chg.	.3046	137	307.78	9.6118	2.1	19	331	326
60			.3046	137	315.675	9.3249		20	333	327
70			.3211	144	322.47	10.0409		21	336	329
80			.3128	140	324.72	9.8513		21	338	331
90			.3210	144	327.06	10.1814		21	342	335
100			.3291	148	329.37	10.5120		22	345	337
110			.3291	148	331.67	10.856		22	350	342
120	↓	↓	.3290	148	333.98	10.656	↓	22	355	347

←---from Part I--->						<Part II>(7x8)				
1	2	3	4	5	6	7	8	9	10	11
PCS	Htg/Clg	Pumps	dV/sec	Equip	K	Rate of	Time for	Press	Appx G	Max
Temp	Rate	Oper-	Cu. ft	gpm		Press	PORV flo	D'sht	Limit	Perm
degF	deg/hr	able				Incras	=Equal	psi	-Temp	Set
						psi/sec	gpm		Press	Pnt
								in sec's	Errors	
130	20	3chg	.3371	151	331,012	10.8211	2.1	23	361	352
140			.3370	151	328,037	10.7207		23	367	358
150			.3369	151	325,062	10.6203		22	375	367
160			.3448	155	322,086	10.7698		23	384	375
170	40		.3515	158	319,111	10.8777		23	339	330
180			.3737	168	316,136	11.4569		24	351	341
190			.3621	162	313,161	10.9968		23	366	357
200			.4042	181	310,186	12.1587		26	383	371
210			.4040	181	303,297	11.8843		25	403	392
220			.4039	181		11.8792		25	426	415
230			.4093	184		12.0447		25	452	441
240	V		.4093	184		12.0388		25	482	471
250	60	V	.4321	194		12.7094		27	471	458
260		3chg	.4404	198		12.9535		27	514	501
260		+24PSI	3.1588	1,418		92.91		195	514	333
270		3chg	.4400	197		12.9418		27	565	552
270		+24PSI	3.1584	1,417		92.8981		195	565	384
280		3chg	.4396	197		12.93		27	623	610
280		+24PSI	3.1580	1,417		92.8863		195	623	442
290		3chg	.4392	197		12.9182		27	681	678
290		+24PSI	3.1576	1,417		92.8746		195	681	510
300		3chg	.4472	201		13.1535		28	740	726
300		+24PSI	3.1656	1,421	V	93.110		196	740	558
310		3chg	.4551	204	242,579	10.7039		22	796	788
310		+24PSI	3.1735	1,424		74.6374		157	796	653
320		3chg	.4545	204		10.6893		22	862	854
320		+24PSI	3.1729	1,424		74.6238		157	862	719
330		3chg	.4540	204		10.6775		22	937	929
330		+24PSI	3.1724	1,424		74.6105		157	937	794
340		3chg	.4534	203		10.6639		22	1,025	1,017
340	V	+24PSI	3.1718	1,424		74.5973		157	1,025	882
350	100	3chg+24PSI	2.6719	1,199		62.8404		132	1,008	890
360			2.309	1,036		54.3043		114	1,107	1,007
370			1.822	818		42.8513		90	1,220	1,144
380			1.3851	622		32.5769		68	1,352	1,298
390			.6227	279	V	19.6456		31	1,504	1,487
400			.6472	290	176,043	11.0492		23	1,680	1,671
410			.6589	296		11.2487		24	1,884	1,874
420			.6727	302		11.4849		24	2,119	2,109
430			.7168	322		12.2370		26	2,390	2,378
440			.7409	333		12.6494		27	2,704	2,691
450		V	.7390	332	V	12.6165		27	3,068	3,055

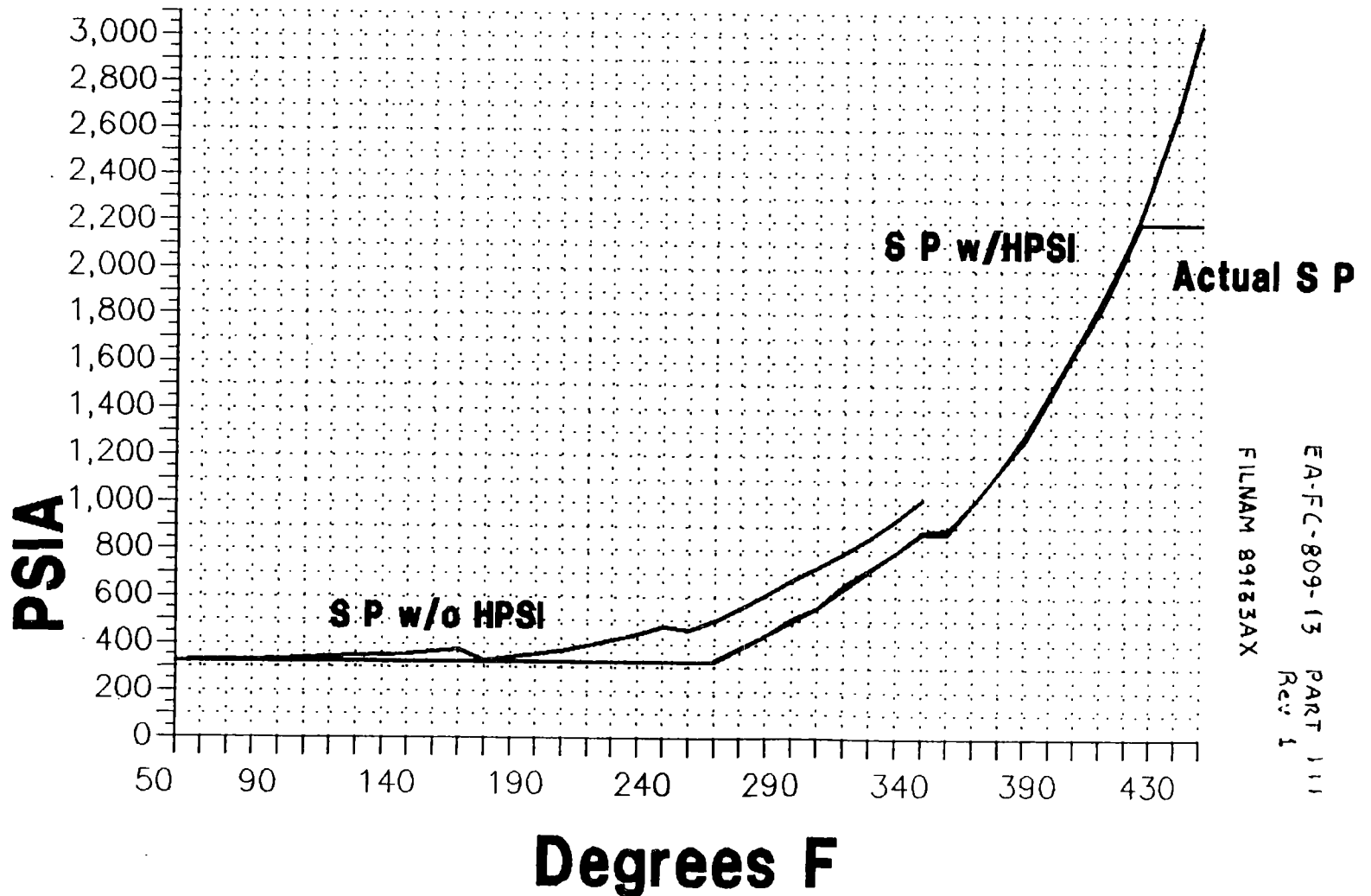
Conclusions:

Attachment 1 graphs the results of these calculations, and illustrates values (Actual Set Point) which will envelope these calculated values.

References:

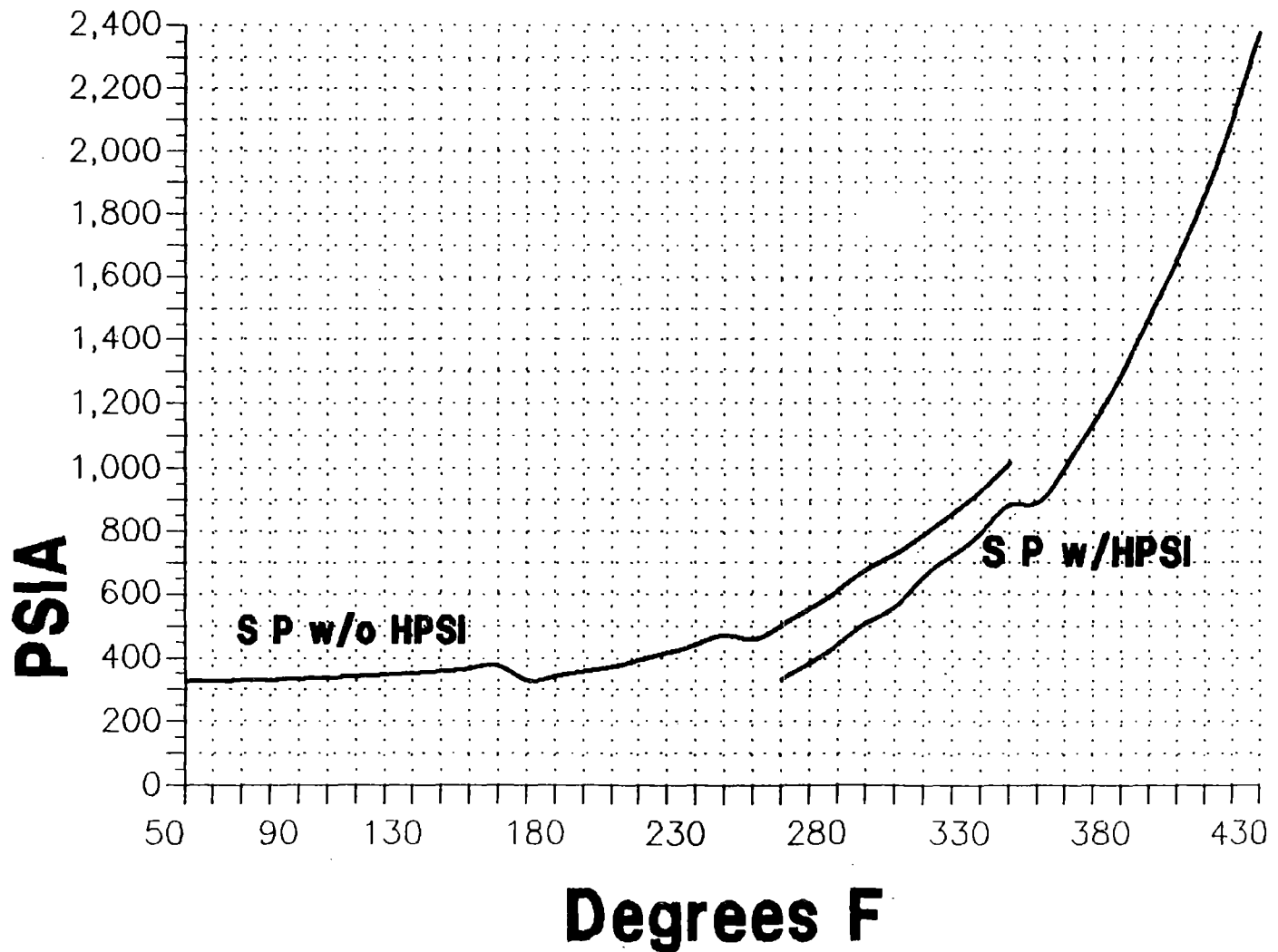
- 1) Target Rock Test Data, Fascimile Transmitted 11 July 1989, 1345
- 2) Target Rock Test Data, Fascimile Transmitted 26 July 1989, 1453
- 3) Combustion Engineering Proposal for Variable Set Point LTOP, Proposal #88-240-AIA, Section II.4, page 6
- 4) EA-A-PAL-89-98, Palisades Pressure and Temperature Limits
- 5) EA-FC-809-19, LTOP Temperature and Pressure Loop Errors
- 6) Letter, L. E. Demick, MPR Asc. Inc, to J.L. Topper, CPCo, 12 September 1989, #98-108-07, COMPUTED STROKE TIMES for PALISADES REPLACEMENT PORVs
- 7) Letter, L. E. Demick, MPR Asc. Inc, to J.L. Topper, CPCo, 18 September 1989, #98-108-09, VALIDATION of DYNAMIC MODELING APPROACH and PROGRAM for the REPLACEMENT PORVs at PALISADES NUCLEAR POWER PLANT

LTOP SETPOINTS



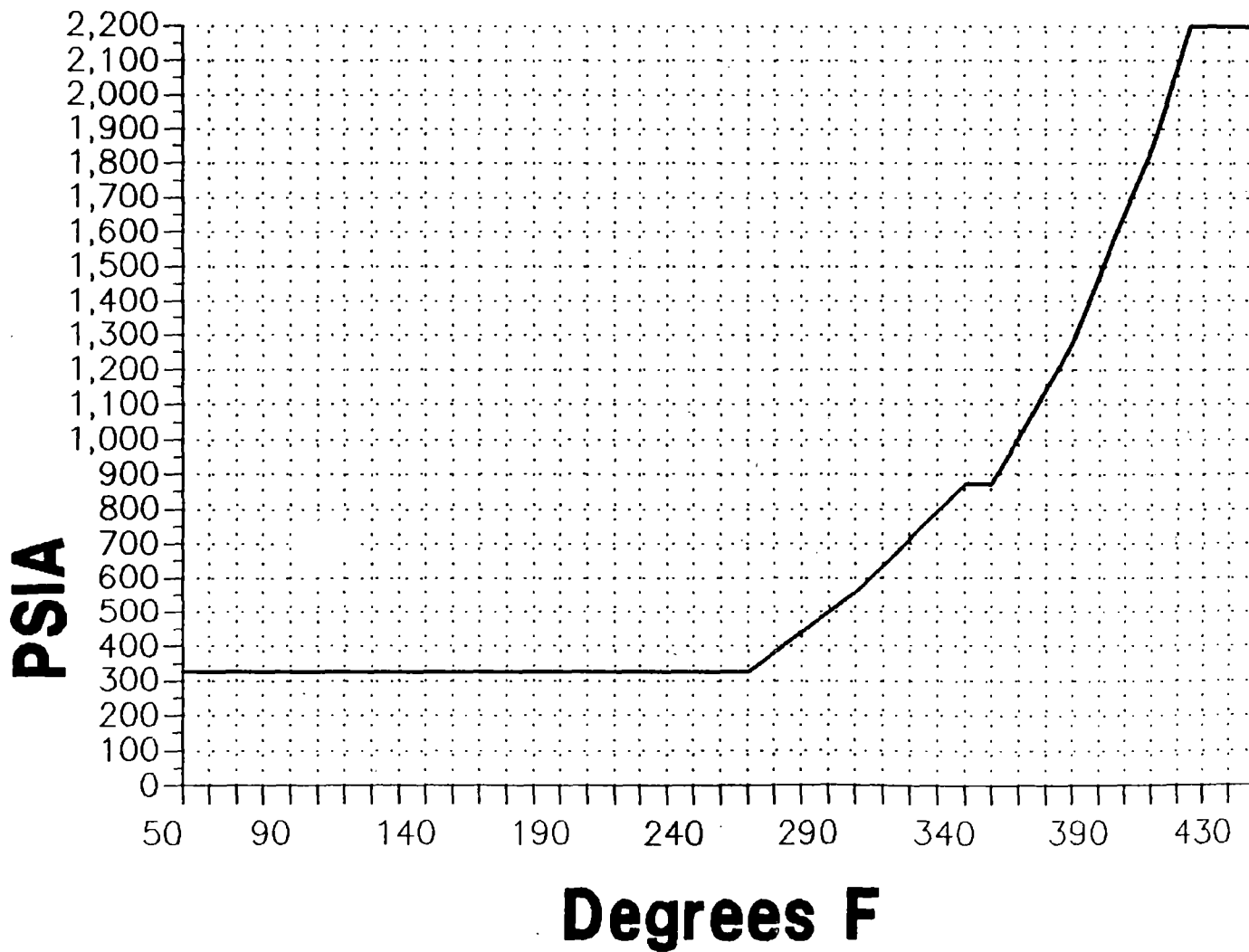
EA-FCL-809-13 PART 111
FILNAM 89123AX
Rev 1

LTOP SETPOINTS



EA-FC-809-13 Part 111
FILNAM 891338r1 Rev 1

ACTUAL LTOP SET POINTS w/SDC ISOLATED



EA-FC-809-13 Part 111
FILMM 8913C-1 Rev 1

ENGINEERING ANALYSIS

Title: Pressure Response Effects of VLTOP with Replacement PORVs
Part IV - Limiting Pressures versus Temperatures for Tech Specs

Objective:

Calculate the pressure at which PORVs must be actuated as a function of PCS temperature to prevent exceeding the applicable Appendix G limit.

Analysis Inputs:

- 1) Pressure overshoot during LTOP actuation, from Part III of this analysis
- 2) Appendix G limits from reference 1

Assumptions:

- 1) PCS heating and cooling rates will be limited to -
 - 20deg/hr at PCS temperatures < 170 deg F
 - 40deg/hr at PCS temperatures from 170 to 250 deg F
 - 60deg/hr at PCS temperatures from 250 to 350 deg F
 - 100deg/hr at PCS temperatures of 350 F and greater
- 2) Pressurizer heating and cooling rates will be 200deg/hr for all PCS temperatures

Calculations:

The following equations define the Appx G limit, as corrected for elevation difference between the limiting RFV weld and the pressurizer, and for the dP created by operation of the Primary Coolant Pumps.

- a) Heating Limited -

$$P_{lim} = (17.206 \times (26.78 + (1.233 \times \text{EXP}(.0145 \times (T - 81 - dT1/4)))) - 54$$

b) Cooling Limited -

$P_{lim} =$

$(17.206 \times (26.78 + (1.233 \times \text{Exp}(.0145 \times (T - 81 + dT1/4)))) - (5.85 \times dT_{max}) - 54$

Where T = PCS temperature, and

dT1/4 for heating	20deg/hr	40deg/hr	60deg/hr	100deg/hr
=	6.3	12.4	18.2	30.0
dT1/4 for cooling				
=	4.4	9.0	13.9	23.6
dTmax for cooling				
=	10.1	20.5	31.8	54

The above equations indicate that cooling is more limiting than heating for temperatures at or below 285 deg F; ie, calculated values from 280 to 290 deg for 60deg/hr rate of change are as follows:

	Heating	Cooling
280	698.6	685.6
281	702.9	692.4
282	707.2	699.2
283	711.6	706.2
284	716.07	713.3
285	720.5932	720.5719
286	725.1	727.8
287	729.8	735.2
288	734.5	742.7
289	739.3	750.4
290	744.1	758.1

Therefore, limiting values will be calculated with the heating equation from 290 degrees and greater, and with the cooling equation from 280 degrees and less.

1	2	3	4	5	6	7
PCS Temp	Rate of Chng	equ. b Limit	equ. a Limit	from Part III Overshoot	LTOP T.S. Limit	Comments
degF		psiG	psiG	psi	psiA	
50	20/hr	362	419	19	357	Overshoot based on initial Per Press of 310 psia
60		364	421	20	358	
70		367		21	360	
80		370		21	363	
90		373		21	366	

0	1	2	3	4	5	6	7
	PCS	Rate	Limit	Limit	Overshoot	LTOP T.S. Limit	Comments
	Temp	of	cooling	heating	w/o HPSI	w/HPSI	
	degF	Chng	psiG	psiG	psi	psi	
						psiA	psiA
	100	20°/hr	377		22		369
	110		382		22		374
	120		387		22		379
	130		394		23		385
	140		401	452	23		392
	150		409	459	22		401
	160		419	468	23		410
	170	40°/hr	375	471	23		366
	180		388		24		378
	190		404		23		395
	200		423		26		411
	210		444		25		433
	220		468		25		457
	230		497		25		486
	240		529	505	25		518
	250	60°/hr	522	596	27		509
	260		569			195	388
	270		623			195	442
	280		686	699		195	505
	290		758	744		195	563
	300			797		196	615
	310			858		157	715
	320			928		157	785
	330			1,009		157	866
	340		1,330	1,103		157	960
	350	100°/hr	1,567	1,085		132	967
	360		1,798	1,191		114	1,091
	370			1,314		90	1,238
	380			1,455		68	1,401
	390			1,619		31	1,602
	400			1,808		23	1,799
	410			2,027		24	2,017
	420			2,280		24	2,270
	427			2,480		25	2,469
	428			2,510		25	2,499
	429			2,541		26	2,529
	430		4,800	2,572		26	2,560

Change in value of K

Initial Press assumed 700 psia
 " " " 900 "
 " " " 1,100 "
 " " " 1,200 "
 " " " 1,400 "

Change K; Press to 1,500 psia
 Press to 1,600 psia

CODE SAFETIES PROTECT
 Press to 1800psia

NOTE:

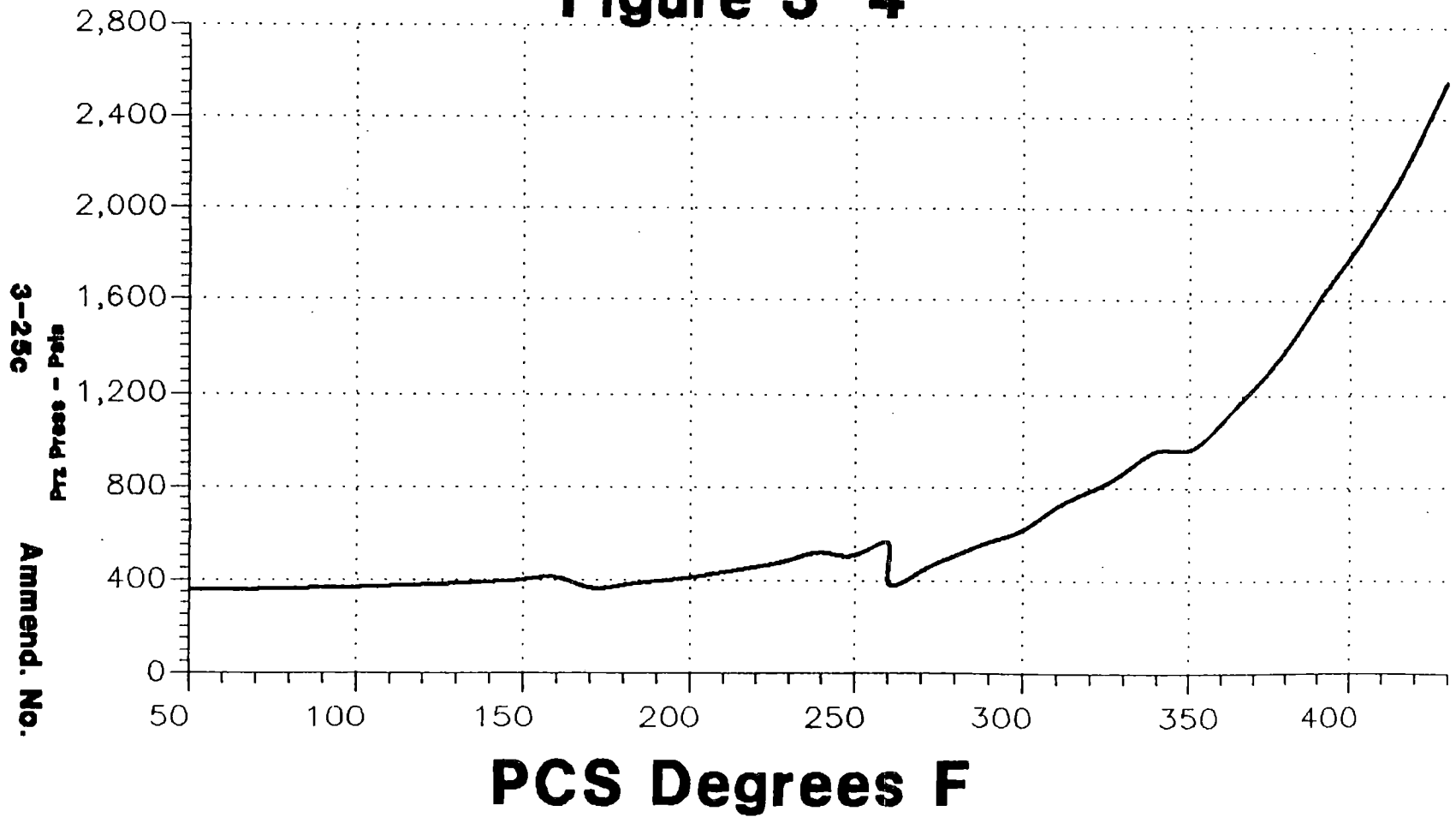
3/4 t values are not limiting for the rates of change of interest, being higher in every instance, for the rates of temperature change assumed, and for the RPV fluence through $1.8E19$ nvt.

References:

- 1) FCS Pressure Temperature limits, August 89 revision, EA-A-FAL-89-98

LTOP LIMIT CURVE

Figure 3-4



3-25c

Prt Press - Ppsi

Ammend. No.

EA-FC-809-13
Part IV Rev 1
FILNAM 89154C-1