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ATTACHMENT B entitled "Change from Inerted to Air Containment Atmosphere (De-Inerted) for Nine Mile Pt. Unit 2 Plant".....

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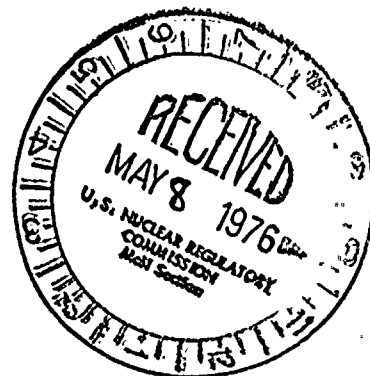
NIAGARA MOHAWK POWER CORPORATION

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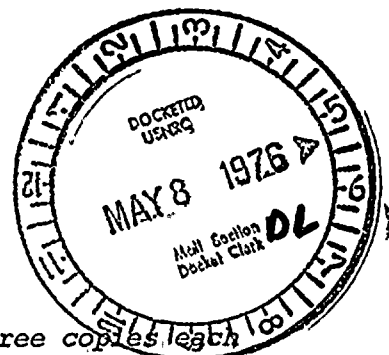
Regulatory Docket File

May 4, 1976



Director of Reactor Regulation
Attn: Mr. J. F. Stolz, Chief
Branch 2-1
U. S. Nuclear Regulatory Commission
Washington, D. C. 20555

Re: Nine Mile Point Unit 2
Docket No. 50-410

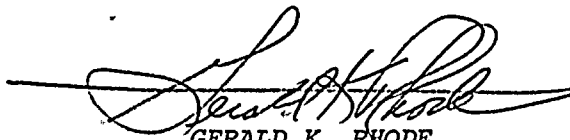


Dear Sir:

Attached for your review and approval are three copies each of the "Main Steam Line Isolation Valve Water Seal Leakage Analysis Abstract and Results" (Attachment A) and "Change from Inerted to Air Containment Atmosphere (De-Inerted)" (Attachment B) for Nine Mile Point Unit 2. Attachment A is submitted in response to Section 9.2.4 of the Commission's Safety Evaluation Report which required certain additional information and analyses. Also, Attachment B provides justification for changing to a de-inerted containment in accordance with Draft Regulatory Guide 1.7, August 1974.

Very truly yours,

NIAGARA MOHAWK POWER CORPORATION



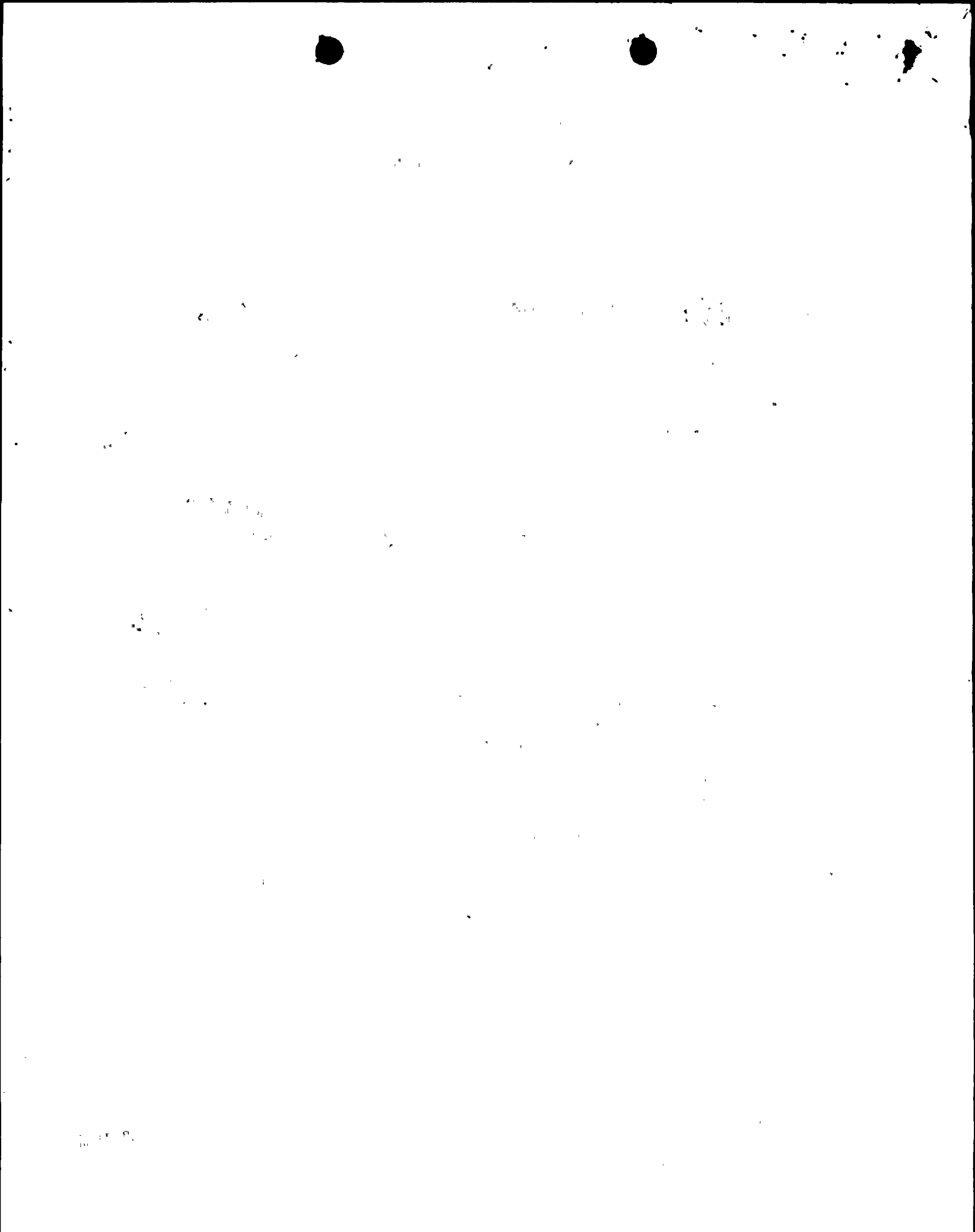
GERALD K. RHODE

Vice President - Engineering

NLR/sz

Attachments

4580



Attachment A

Regulatory Docket File

MAIN STEAM LINE ISOLATION VALVE
WATER SEAL LEAKAGE ANALYSIS
ABSTRACT AND RESULTS

NINE MILE POINT NUCLEAR STATION - UNIT 2
NIAGARA MOHAWK POWER CORPORATION

Docket No. 50-410

~~Regulatory Docket~~ 5-4-76

April, 1976

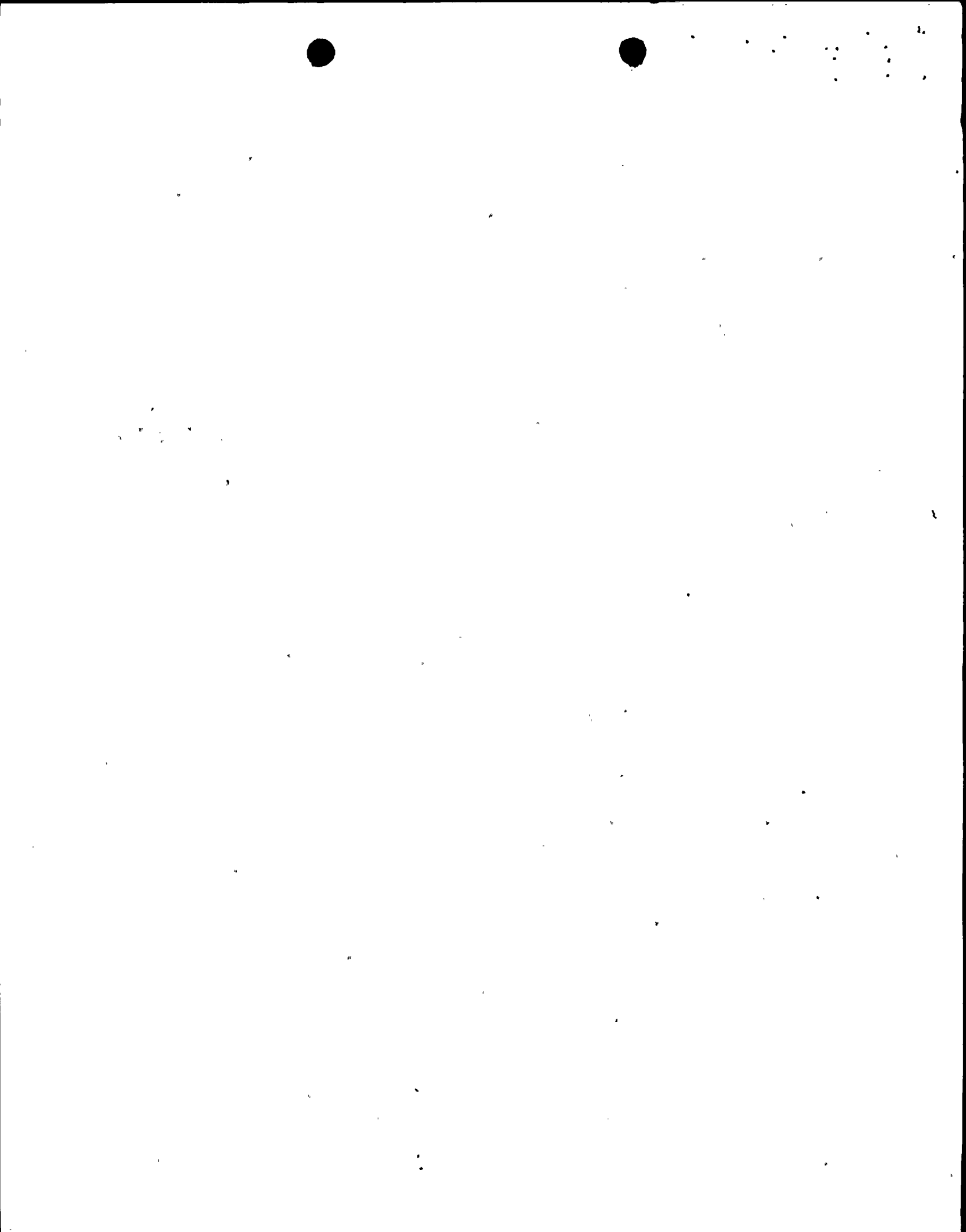


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LIST OF FIGURES

- Figure 1 Typical Main Steam Line Isolation Valve
- Figure 2 Leakage Area and Gap Width Variation
- Figure 3 ΔT and Leak Rate vs. Time



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1.0 INTRODUCTION

The purpose of this report is to provide a description of the leakage analysis and orientation of the main steam isolation valves to be installed at Nine Mile Point Nuclear Station - Unit 2. This analysis is submitted in response to Section 9.2.4 of the Commission's Safety Evaluation Report.^{1,2} The results of the full analysis of the valve and water seal system will be contained in the Final Safety Analysis Report.

2.0 DISCUSSION

An analysis was performed to determine the water leakage rate and thermal stress levels of a typical main steam isolation valve (shown in Figure 1) considering valve component temperature distribution and actuator forces during operation of the water seal system.³

The valve used in this report is a 26-inch diameter, Y-pattern globe valve⁴ with its cylindrical poppet and disc moving on a centerline 45 degrees to the steam flow direction. All main steam line isolation valves will be mounted in 45 degree pipe runs (see Figure 1 and 3) so that the valve stem is vertical. This is an improvement from the orientation described in the Preliminary Safety Analysis Report.⁵ The improved orientation meets all code requirements and the stress and fatigue limits for piping between isolation valves described in Mechanical Engineering Branch Technical Position 3-1".⁶ The vertical valve stem orientation results in the following advantages:

1. Reduced Personnel Exposure

With a vertical stem and operator, the main steam line isolation valve is significantly easier to maintain, thus reducing personnel exposure during maintenance.

2. Improved Operability

With the stem movement vertical, friction forces will be reduced, and, consequently, valve operability will be improved.

3. Reduced Maintenance Costs

Reduced maintenance time will result in cost savings over the life of the plant.

This analysis of the typical valve is conservative in that the assumed clearances around the poppet (between the poppet and the body) are small at $\theta_1 = 0$ degrees (see Figure 1). The assumed clearance results in a severe flow restriction of seal water to the downstream side of the valve poppet and, therefore, a higher temperature differential across the poppet.



3.0 ANALYTICAL METHOD

The major assumptions used in the analysis are:

Seal water at 100 F is injected into the MSLIV through the warm-up drain connection with the valve at an equilibrium temperature of 546 F. Actual seal water temperature will be somewhat lower (70-100 F), and the lower temperature will be factored into the final analysis. However, the effect on the results is expected to be insignificant.

The maximum valve actuator force is 30,000 lbs.

During seal water injection, the differential pressure across the valve disc remains at 50 psi.

The hard-faced sealing surfaces of the valve disc and seat have only point contact at the location $\theta_1 = 0$ degrees for all cases of thermal distortion and application of the actuator load.

The valve is closed with essentially zero leakage occurring before the 100 F water injection.

The inner isolation valve is analyzed for leakage with the outer isolation valve considered to have failed in the open position.

An elastic analysis is applicable.

Seal water injection flow rate is 70 to 80 gpm.

A heat transfer analysis of the valve body and disc was performed to determine temperature distribution as a function of time during seal water injection into the hot valve. During this period, one side of the valve body, poppet, and disc ($\theta_2 = 180$ degrees) is cooled by a larger pool of water than the opposite ($\theta_1 = 0$ degrees) side. The major heat transfer mechanism for the side cooled by the larger pool of water is nucleate boiling during most of the thermal shock transient. The heat transfer mechanism for the opposite side is stable film boiling due to the more restrictive circulation path for seal fluid. Heat transfer coefficients were calculated based on the references listed in footnotes 10 and 11.

Temperature distributions in the body and poppet were obtained by the "LION" heat transfer computer code⁷ in the form,

$$T(r,z,\theta,t) = TF1(r,z,t) + TF2(r,z,t)\cos\theta.$$

Where r = Radial location
 z = Axial location
 θ = Circumferential location
 t = Time



At any time $T(r,z,0,t)$ gives the r-z plane temperature distribution due to stable film boiling. $T(r,z,180,t)$ gives the r-z plane temperature distribution due to convective nucleate boiling on the opposite side of the valve. These temperature distributions versus time were input into separate finite element models of the valve body and disc. Thermal distortions were determined with the ASAAS computer program.⁸ The ASAAS program was also used in performing thermal stress analyses. Displacements of the valve disc and body, due to actuator seating forces applied to the valve stem, were calculated using ASAAS and SHELL 1⁸ computer codes.

The leakage area due to differential thermal growth and the actuator seating force is shown in Figure 2. The maximum gap width, G_{max} , was obtained by considering the radial and axial relative motions of the valve disc and body at $\theta_1 = 0$ and $\theta_2 = 180$ degrees. The gap width variation around the circumference is expressed as $G(\theta) = G_{max} \sin \theta/2$ as shown in Figure 2. The total leakage of injection water from the main steam line isolation valve was calculated based on the area of this gap between the valve disc and the body.

Using the methods described above, the peak valve leakage was determined to be 26.4 gpm, 7 minutes following seal water injection. Leakage rate as a function of time is shown in Figure 3. Valve stresses are within the allowable limits.⁹

4.0 CONCLUSIONS

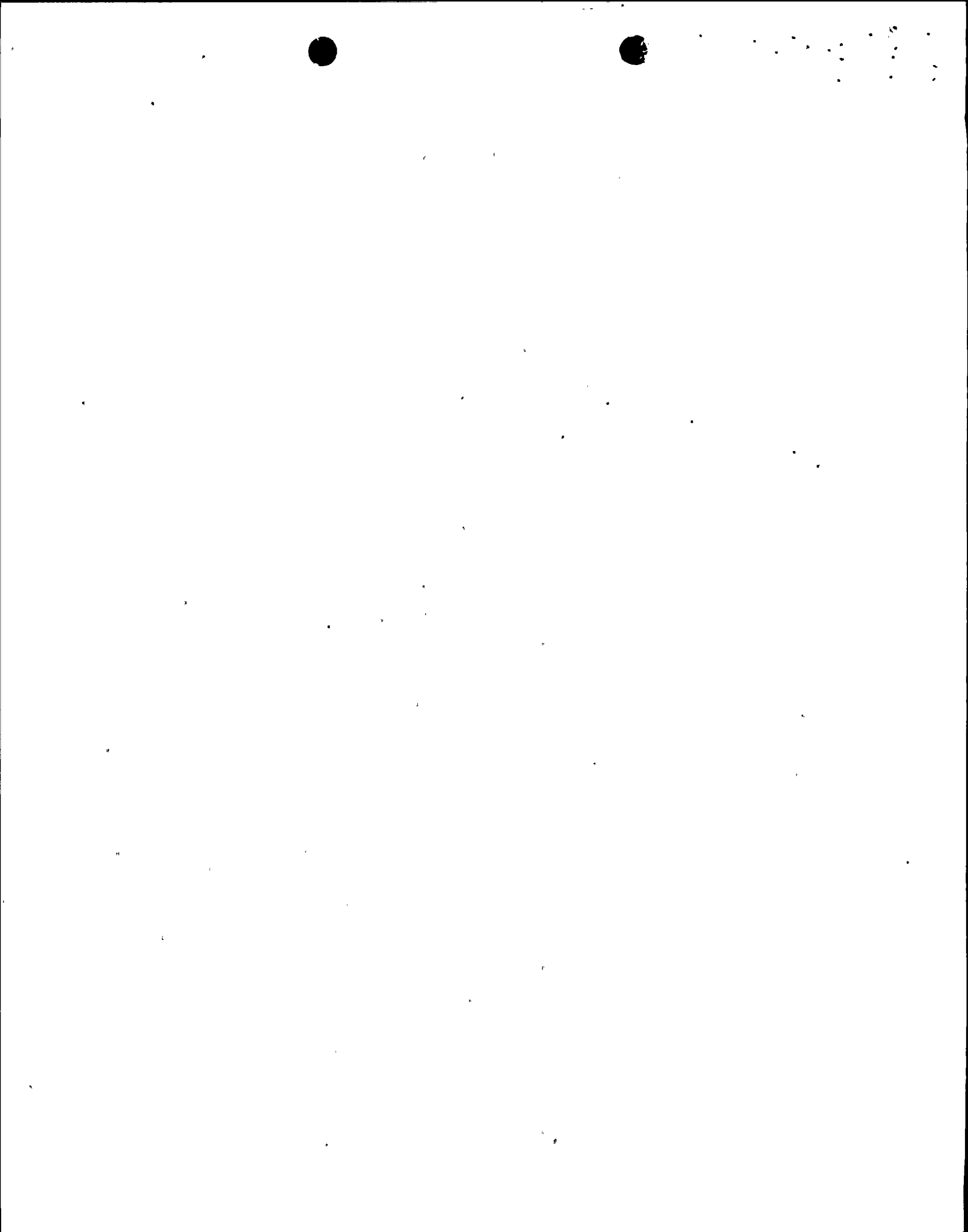
Since the peak leakage rate of 26.4 gpm is lower than the injection rate (70 - 80 gpm), a water seal will be maintained. Valve leakage will be steam produced due to the flashing of spent fuel pool water rather than steam from the reactor vessel.

Footnotes:

1. Safety Evaluation of the Nine Mile Point Nuclear Station - Unit 2 (SER), June 15, 1973.
2. SER, Supplement 1, August 7, 1973.
3. Nine Mile Point Nuclear Station - Unit 2 Preliminary Safety Analysis Report (PSAR) Chapter 10 Section 10.16.
4. "Design and Performance of GE Boiling Water Reactor Main Steam Isolation Valve" Report No. APED-5750, General Electric Co., March, 1969.
5. PSAR Chapter 4 Section 4.5.3.



6. Branch Technical Position MFB 3-1, "Protection Against Postulated Piping Failures in Fluid Systems Outside Containment."
7. "LION" Computer Code "Temperature Distribution for Arbitrary Shapes and Arbitrary Spaces and Complicated Boundary Conditions," J. R. Schmid, et al, GE-KAPL, KAPL-M-6532 (EC-57,) July 27, 1966.
8. PSAR Appendix C Response C7.6.
9. American Society of Mechanical Engineers, Boiler and Pressure Vessel Code, Section III, Div. I, Nuclear Power Plant Components, 1974, paragraph NB 3222.2.
10. Heat, Mass and Momentum Transfer, Rohsenow & Choi, Prentice-Hall, 1961.
11. Heat Transmission, W. H. McAdams, McGraw-Hill, 1954.



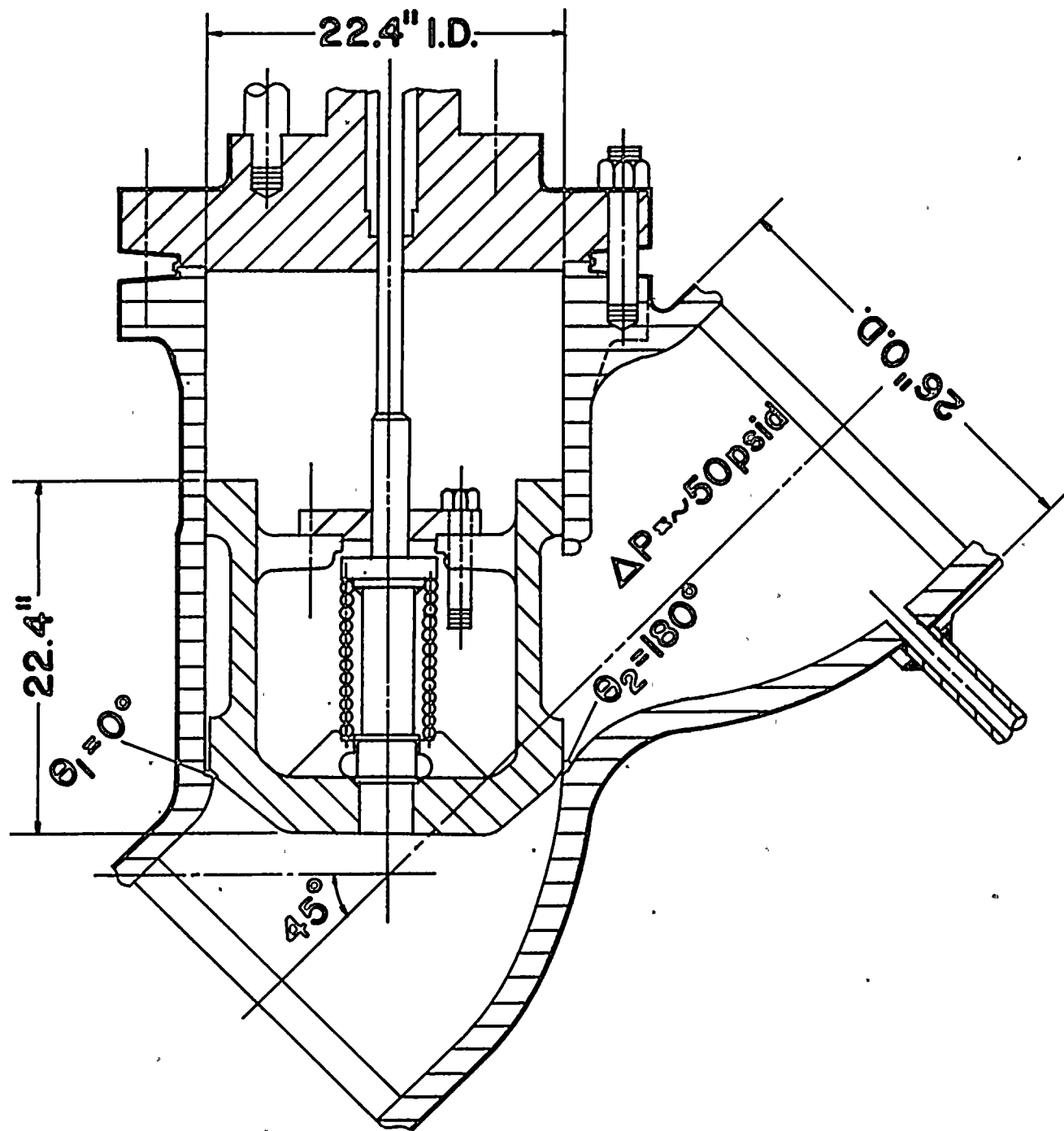


Figure 1
TYPICAL MAIN STEAM
ISOLATION VALVE

NINE MILE POINT NUCLEAR STATION, UNIT 2
 NIAGARA MOHAWK POWER CORPORATION

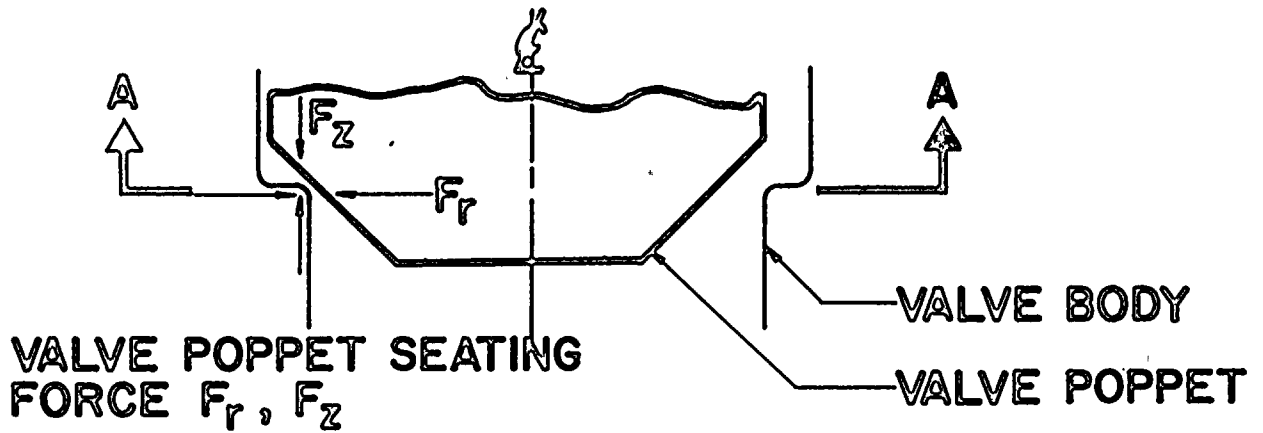
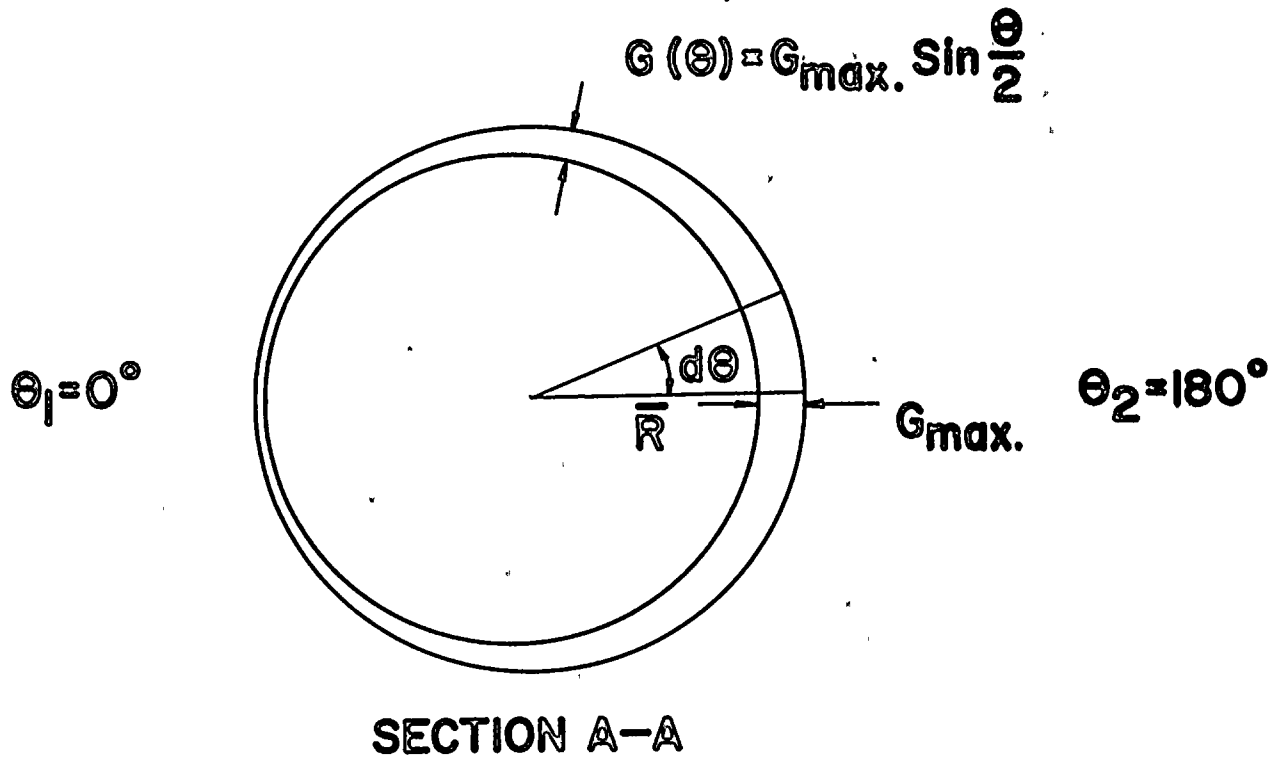


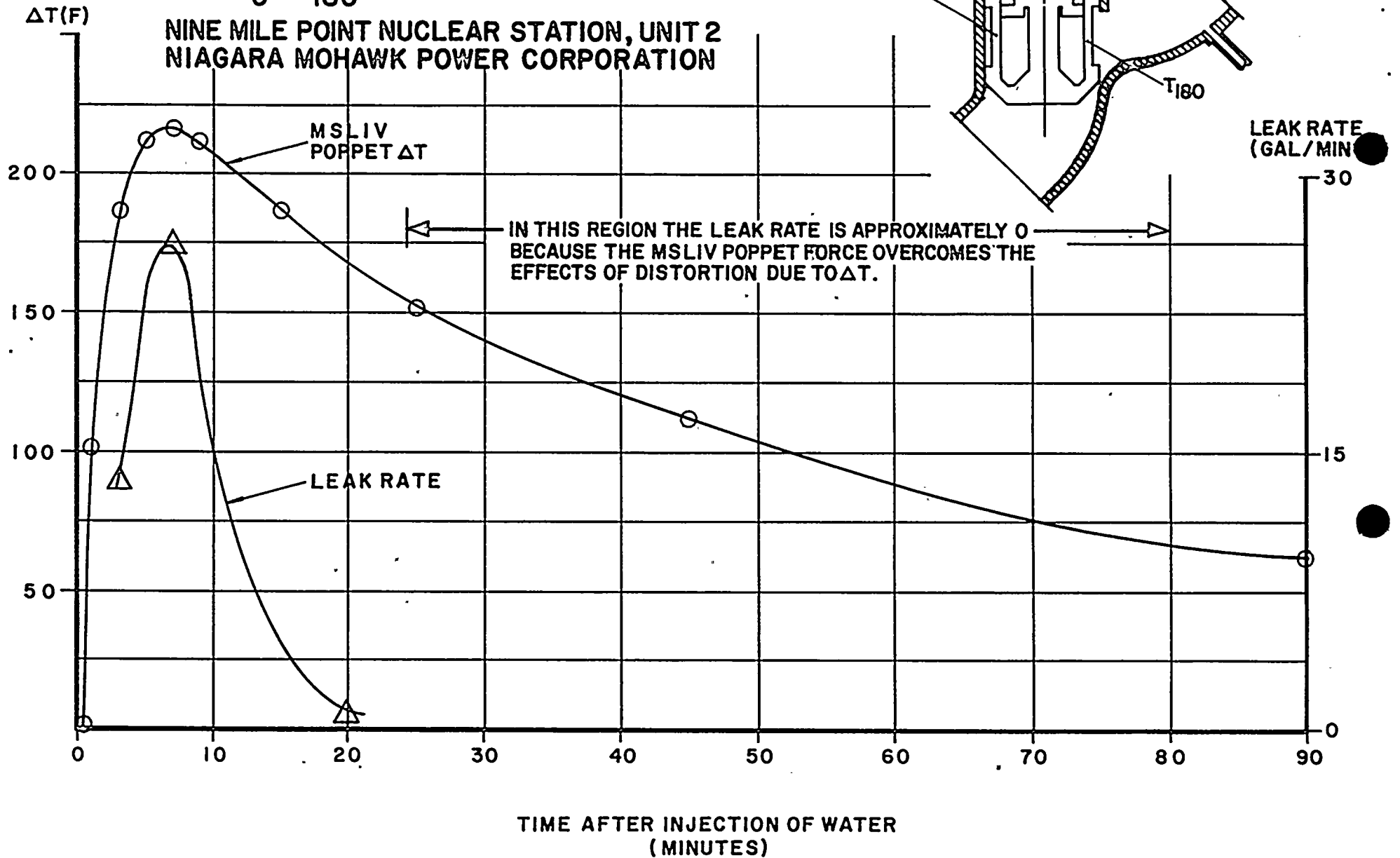
Figure 2
LEAKAGE AREA AND GAP WIDTH VARIATION
 NINE MILE POINT NUCLEAR STATION, UNIT 2
 NIAGARA MOHAWK POWER CORPORATION



Figure 3
 ΔT AND LEAK RATE vs. TIME

$\Delta T = T_0 - T_{180}$

NINE MILE POINT NUCLEAR STATION, UNIT 2
NIAGARA MOHAWK POWER CORPORATION





Attachment B

Regulatory Docket File

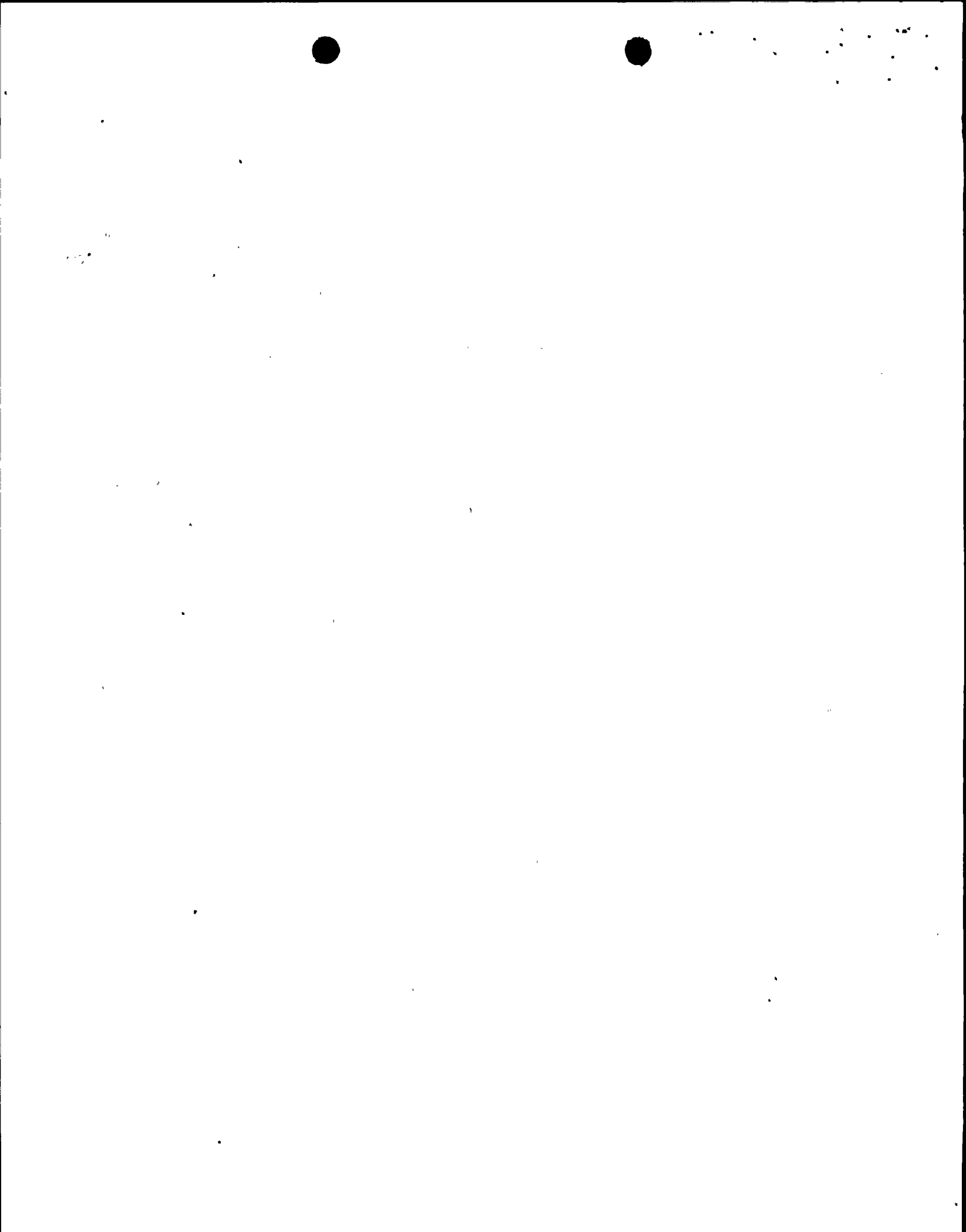
CHANGE FROM INERTED TO AIR CONTAINMENT
ATMOSPHERE (DE-INERTED)

~~Regulatory Docket~~ 5-4-76

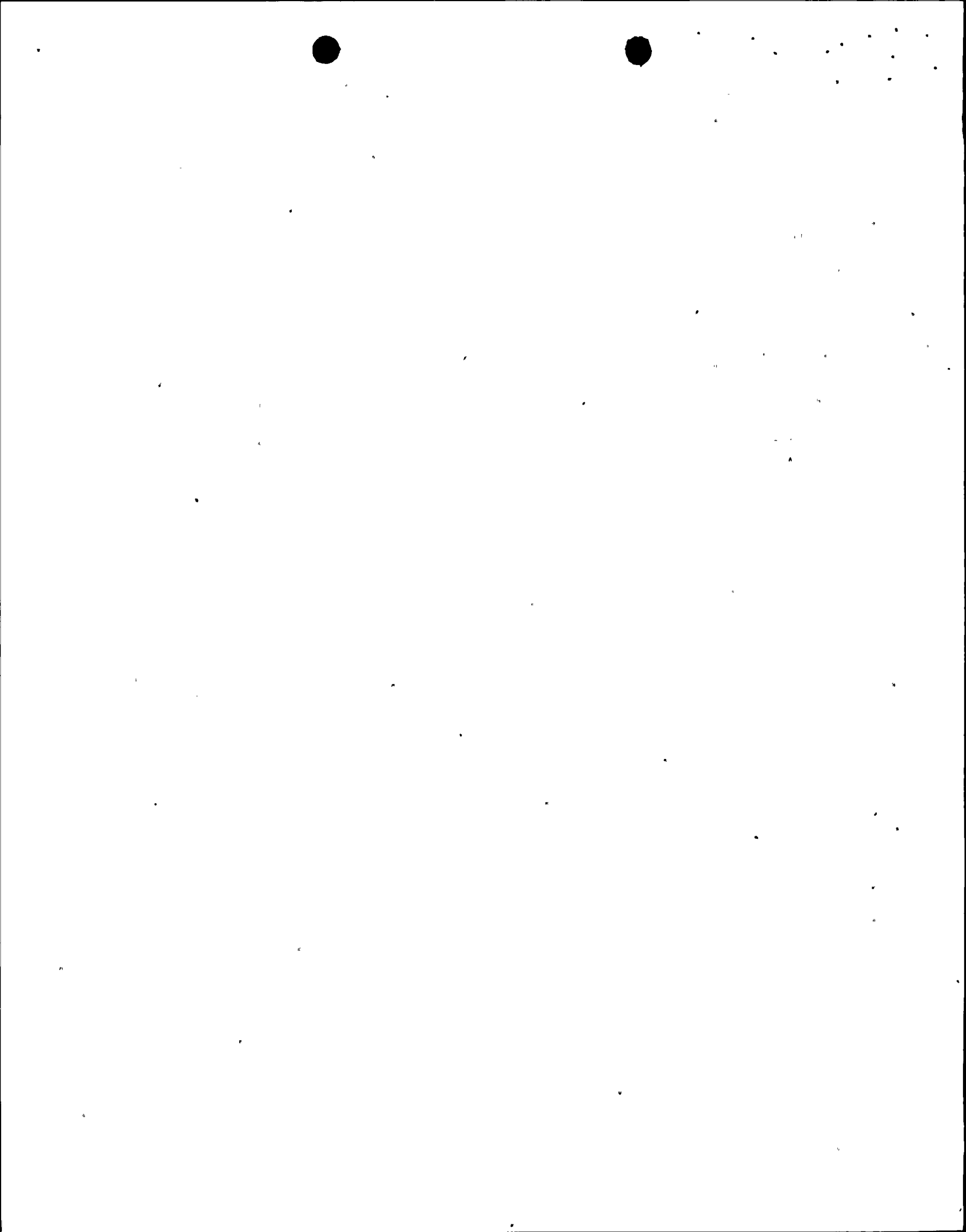
NINE MILE POINT NUCLEAR STATION - UNIT 2
NIAGARA MOHAWK POWER CORPORATION

Docket No. 50-410

April, 1976

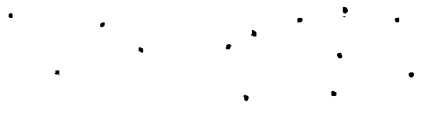


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- Figure 4 Air Addition Rate for Purge System To Maintain Hydrogen
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- Figure 5 Primary Containment Pressure With Purge Operation .



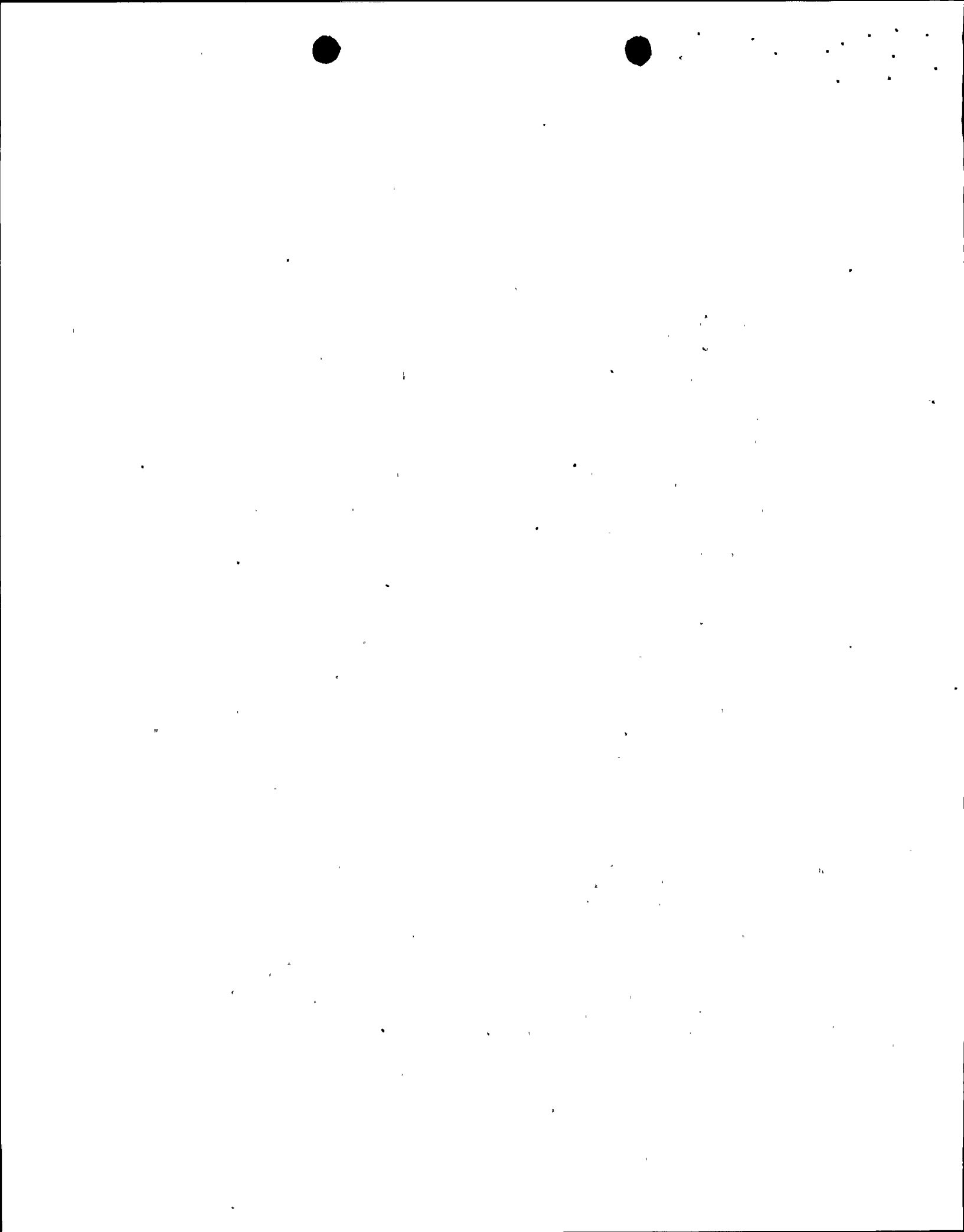
1.0 INTRODUCTION

This report describes the analysis of hydrogen generation due to a loss of coolant accident for Nine Mile Point - Unit 2. The report compares hydrogen control utilizing a hydrogen recombiner and an air purge system for both inerted and noninerted containments. This submittal is provided to justify changing from an inerted primary containment to a noninerted containment. This change does not compromise safe control of the flammable mixtures of hydrogen and oxygen produced during a loss of coolant accident. A noninerted containment is desirable because it simplifies the control of concentrations of flammable mixtures and eliminates the safety hazards associated with residual nitrogen in the containment.

Several disadvantages of an inerted containment may be summarized as follows:

1. Entry of working personnel into an inerted containment requires special breathing apparatus and may be hazardous.
2. Reduced inspection capability due to time spent in determining hazardous residual concentrations of nitrogen after deinerting the containment.
3. Additional radiation exposure resulting from the recognized need to locate possible nitrogen pockets.
4. An inerted containment may require a recombiner with a recycle stream and provision to add oxygen at the recombiner inlet. This involves more equipment and controls, increasing maintenance, and reducing reliability.

Regulatory Guide 1.7 (1) originally specified that, following a loss of coolant accident, a five percent metal cladding/water reaction was assumed to occur. Draft 2 of Regulatory Guide 1.7 (2) and Branch Technical Position CSB 6-2 (3) have altered the basis for determination of hydrogen generation. This results in substantially lower calculated hydrogen generation following a loss of coolant accident.



2.0 DISCUSSION

The present hydrogen control system consists of redundant Seismic Category I recombiner systems with a non-safety related standby air purge system to be used as a backup system. Each recombiner system takes suction from either the drywell or suppression chamber or both and returns hydrogen-free air to the suppression chamber.

The air for the standby purge system is introduced into the containment from the service air system. Initially, air is added which reduces hydrogen concentration and allows containment pressure to rise without releasing to the atmosphere. In this manner, radioactive contaminants are held as long as possible. When the pressure rises to approximately 38 psig, air will be released through a filtration system to the atmosphere. Air will also be added to the primary containment to keep hydrogen concentration below four percent while not exceeding 38 psig.

Of the two alternative criteria used by the Branch Technical Position for determining the performance of the hydrogen control system, it is expected that the one percent metal cladding/water reaction will govern. However, hydrogen is continued to be generated after the initial metal/water reaction due to the radiolytic decomposition of water and is shown as a function of time after loss of coolant accident in Figure 1.

Calculation under Code of Federal Regulations, Title 10, Part 50, Section 50.46 (4) should result in a reaction of less than 0.2 percent of the cladding mass. When this mass is multiplied by five (3) the resultant mass of reaction should not exceed one percent. Verification of the assumption of a one percent reaction for this analysis will be provided in the Final Safety Analysis Report, when calculations under Code of Federal Regulations, Title 10, Part 50, Section 50.46 are available.

The analysis, the results of which are summarized below, determines that one one-hundred standard cubic foot per minute hydrogen recombiner, started within twenty-four hours after loss of coolant accident will hold the hydrogen concentration below four percent. The calculations analyze hydrogen generation rate and recombiner performance and tabulate the gaseous composition of the containment versus time.

3.0 SUMMARY OF ANALYSIS

Parameters

The calculations were based upon all parameters in Regulatory Guide 1.7 (1) as well as the specific project parameters listed below:

- | | |
|---|-------------------------|
| 1. Reactor power (105 percent of rated) | 3489 Mwt |
| 2. Drywell volume | 340,900 ft ³ |



3.	Suppression chamber volume (at high' water level)	200,600 ft ³
4.	Initial drywell pressure	15.45 psia
5.	Initial drywell temperature	135 F
6.	Initial drywell dew point	80 F
7.	Initial suppression chamber pressure	15.45 psia
8.	Initial suppression chamber temperature	90 F
9.	Initial suppression chamber dew point	90 F
10.	Weight of zirconium in outermost 23 mils of active fuel cladding (not including plenum space).	56,486 lbs

Assumptions

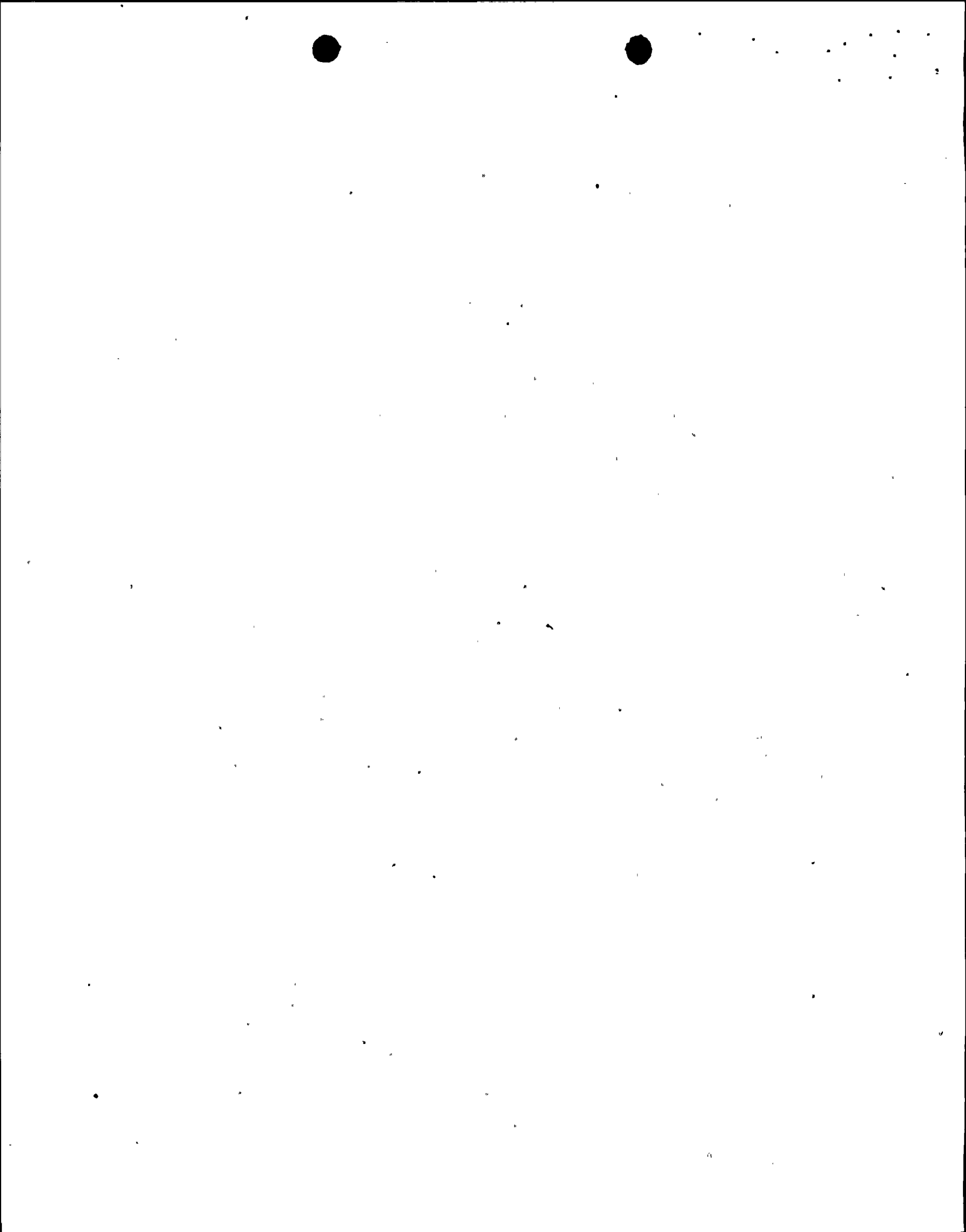
1. Recombiner draws from the drywell and returns hydrogen-free gas to the suppression chamber.
2. Water vapor partial pressure is neglected in the calculation of percent volume of H₂, O₂, N₂ (percent volume dry).
3. Containment atmosphere is 21 percent oxygen initially if non-inerted and four percent initially if inerted.

Results

1. 100 scfm recombiner; noninerted containment.

	<u>Composition</u> <u>at start (24 hrs)</u>		<u>Composition at peak</u> <u>H₂ conc. (56 hrs)</u>	
	Volume percent		Volume percent	
	<u>Dry</u>	<u>Wet</u>	<u>Dry</u>	<u>Wet</u>
H ₂	3.2	2.7	3.9	3.5
O ₂	21.0	17.8	21.3	18.8
N ₂	75.8	64.3	74.8	65.8
H ₂ O	--	15.2	--	11.9

See Figures 2 and 3.



2. 100 scfm recombiner; inerted containment.

	<u>Composition</u> <u>at start (24 hrs)</u>		<u>Composition at peak</u> <u>H₂ Conc. (56 hrs)</u>	
	Volume percent		Volume percent	
	<u>Dry</u>	<u>Wet</u>	<u>Dry</u>	<u>Wet</u>
H ₂	3.2	2.7	3.9	3.5
O ₂	4.7	4.0	5.2	4.6
N ₂	92.1	78.1	90.9	79.9
H ₂ O	--	15.2	--	12.0

3. A purge system adding air to noninerted containment.

Start - 40 hrs after LOCA
Maximum pressure - 38 psig @ 18 days
Maximum addition rate - 84 scfm
Total air added - 960,000 SCF

See Figures 4 and 5.

The above results indicate a margin of conservatism in the control of hydrogen:

1. The analysis was performed to limit the hydrogen concentration to below four volume percent, calculated neglecting water vapor. If the percent volume is computed considering water vapor, the hydrogen concentration is held below 3.5 percent.
2. If the recombiners were started before 24 hours, a lower maximum value of hydrogen concentration would result.
3. The flow rate through the recombiner could be increased to reduce hydrogen concentration further.

The effect of various recombiner capacities can be determined for both the inerted and noninerted cases. The results show that the hydrogen concentration versus time is unaffected by whether or not the containment is initially inerted. For the noninerted case, Figures 2 and 3 plot hydrogen concentration versus time after a loss of coolant accident with and without the recombiner system. Additionally, the effect of a



nonsafety-related air purge system as a backup to the recombiner system was analyzed, and it was determined that the hydrogen concentration could be held below four percent if purging is begun within forty hours after a loss of coolant accident. Figure 4 shows the air addition rate versus time necessary to maintain the hydrogen concentration below four percent.

4.0 CONCLUSIONS

The analysis indicates that the requirements of Branch Technical Position Section 7.d. (3) and Regulatory Guide 1.7 specifying the criteria for hydrogen generation and the allowable limits of hydrogen concentration, are met by employing a redundant hydrogen recombiner and a noninerted atmosphere and by monitoring and controlling hydrogen concentration while allowing the oxygen level to remain at normal air concentration. Elimination of the need to control oxygen results in less equipment and increased system reliability. The noninerted containment eliminates the potential safety hazards associated with the presence of residual nitrogen when the containment is entered.

Footnotes

- (1) Nuclear Regulatory Commission, Regulatory Guide 1.7 (Safety Guide 7), March, 1971
- (2) Nuclear Regulatory Commission, Regulatory Guide 1.7 "Control of Combustible Gas Concentration in Containment Following a Loss of Coolant Accident" - Draft 2, August, 1974
- (3) Nuclear Regulatory Commission, Branch Technical Position CSB 6-2, "Control of Combustible Gas Concentrations in Containment following a Loss of Coolant Accident", March, 1975
- (4) Code of Federal Regulations, Title 10, Part 50, Section 50.46, "Acceptance Criteria for Emergency Core Cooling System for Light Water Nuclear Power Reactors."

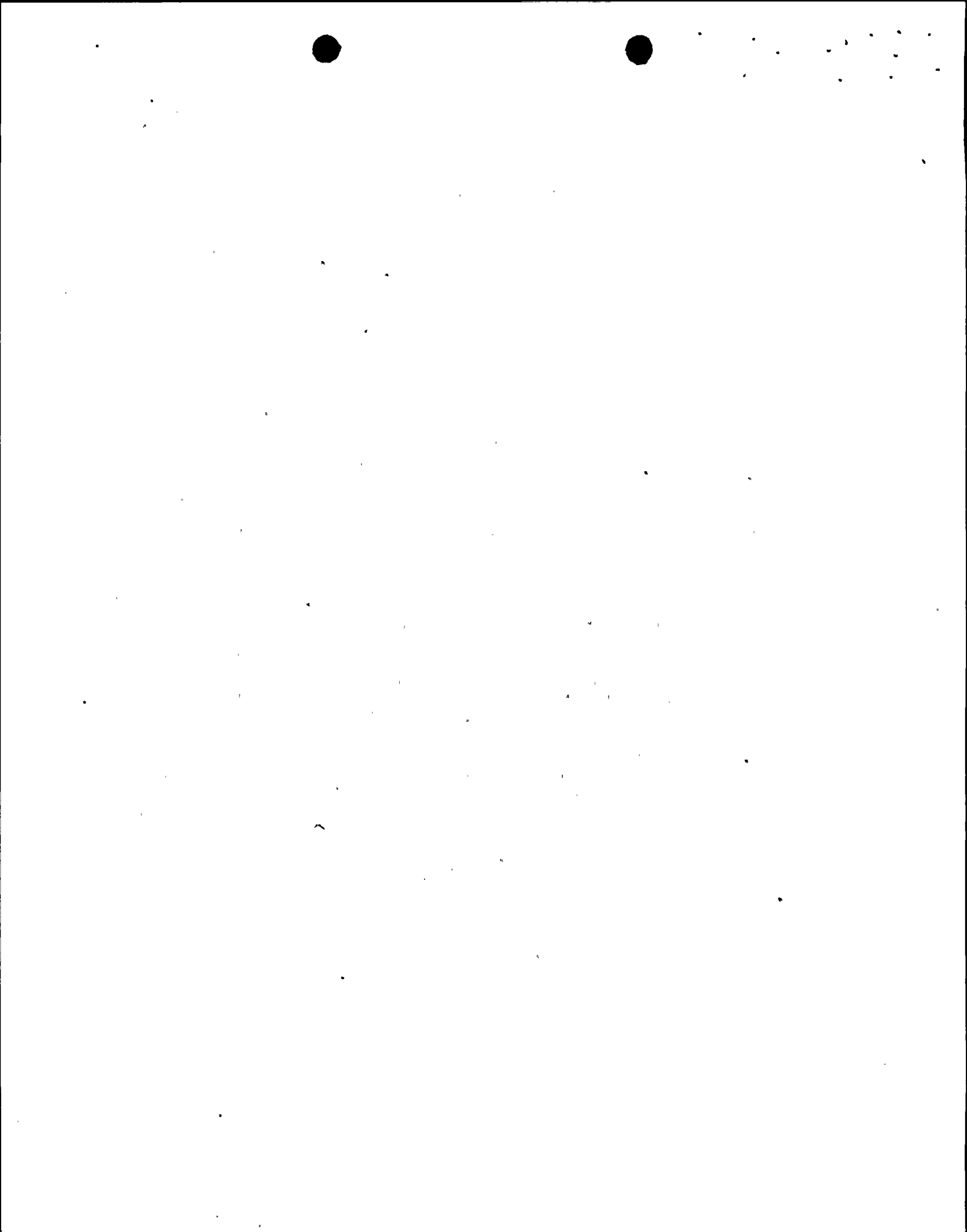
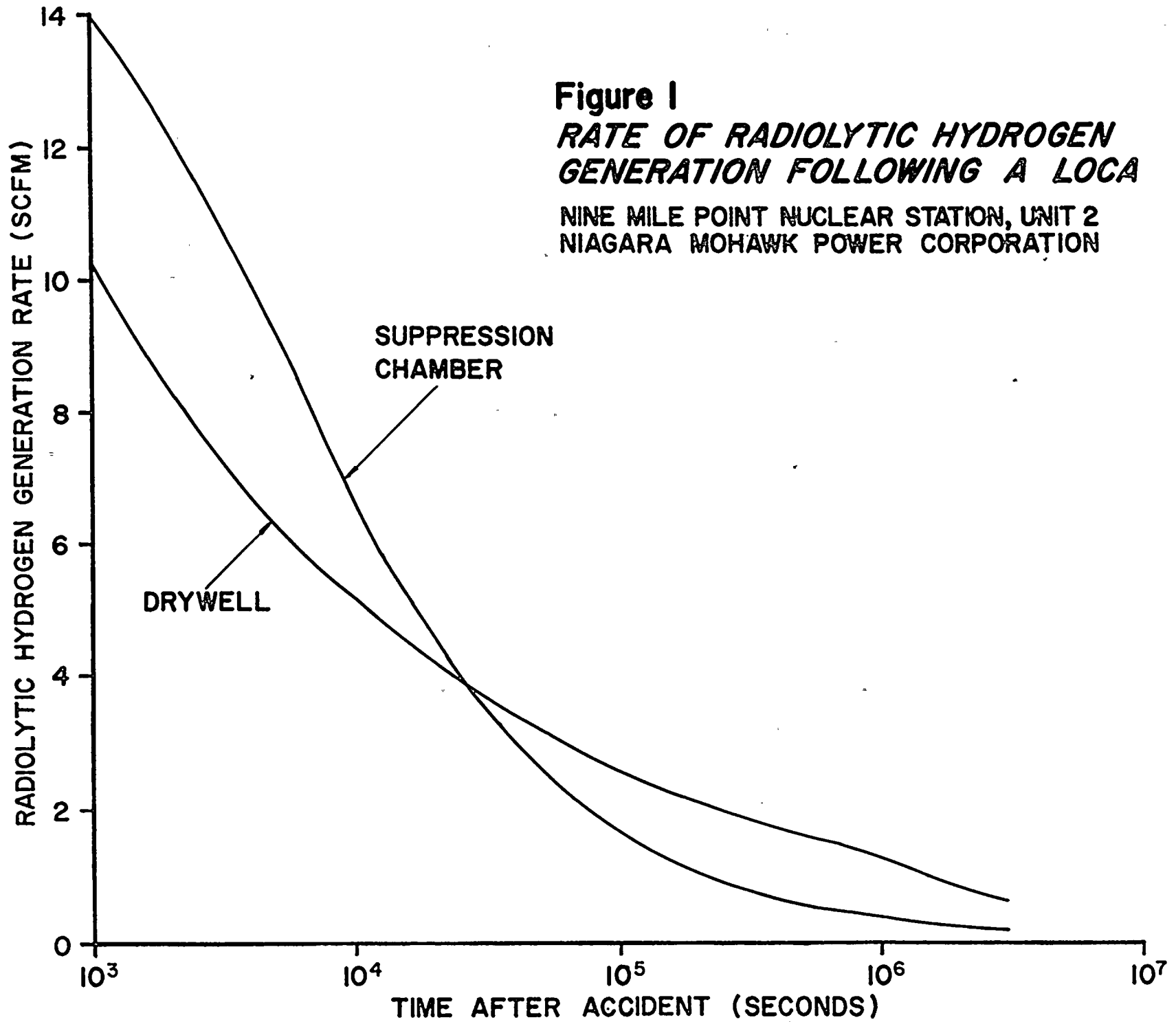


Figure 1
RATE OF RADIOLYTIC HYDROGEN
GENERATION FOLLOWING A LOCA

NINE MILE POINT NUCLEAR STATION, UNIT 2
NIAGARA MOHAWK POWER CORPORATION



REPUBLICAN PARTY (DEMOCRATIC) POLITICAL GROUP

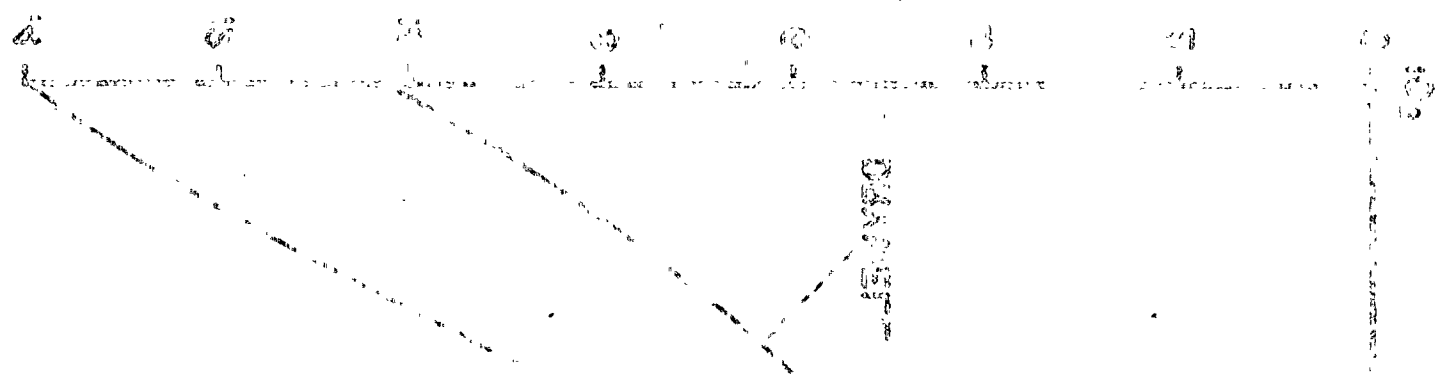
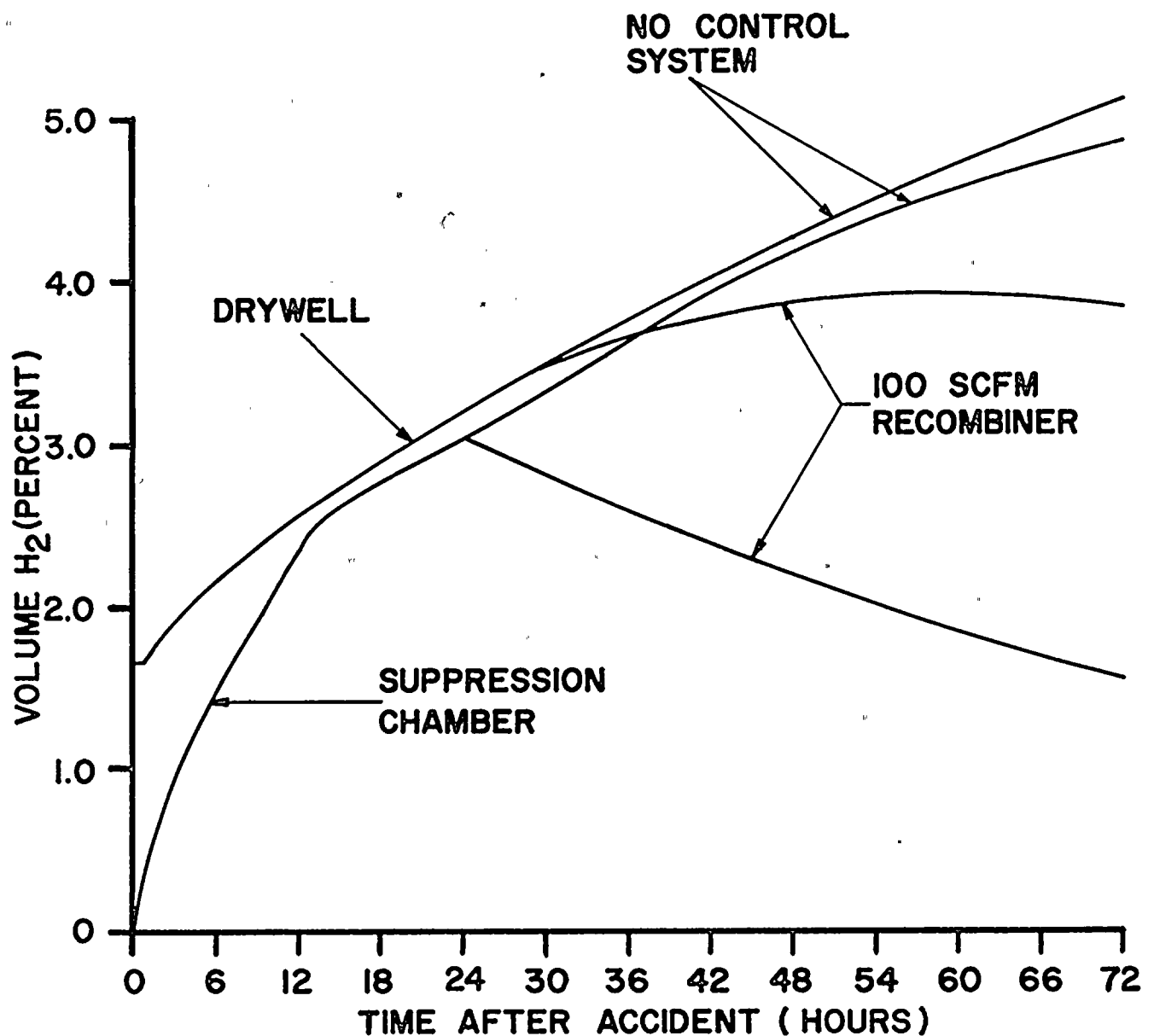


Figure 2

**HYDROGEN CONCENTRATION IN PRIMARY
CONTAINMENT FOLLOWING A LOCA-SHORT
TERM WITH 100 SCFM RECOMBINER**

**NINE MILE POINT NUCLEAR STATION, UNIT 2
NIAGARA MOHAWK POWER CORPORATION**



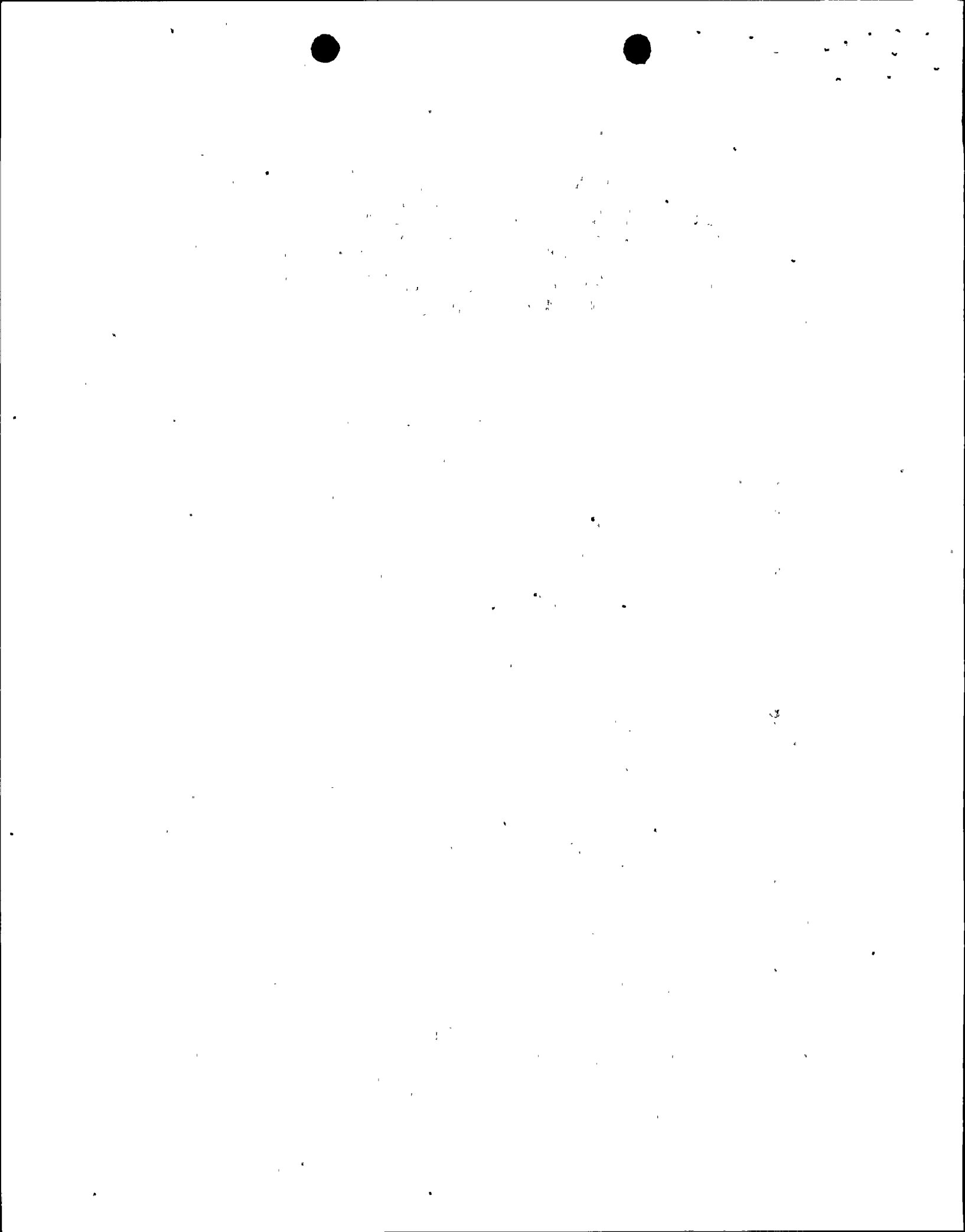


Figure 3

**HYDROGEN CONCENTRATION IN
PRIMARY CONTAINMENT FOLLOWING
A LOCA-LONG TERM**

**NINE MILE POINT NUCLEAR STATION, UNIT 2
NIAGARA MOHAWK POWER CORPORATION**

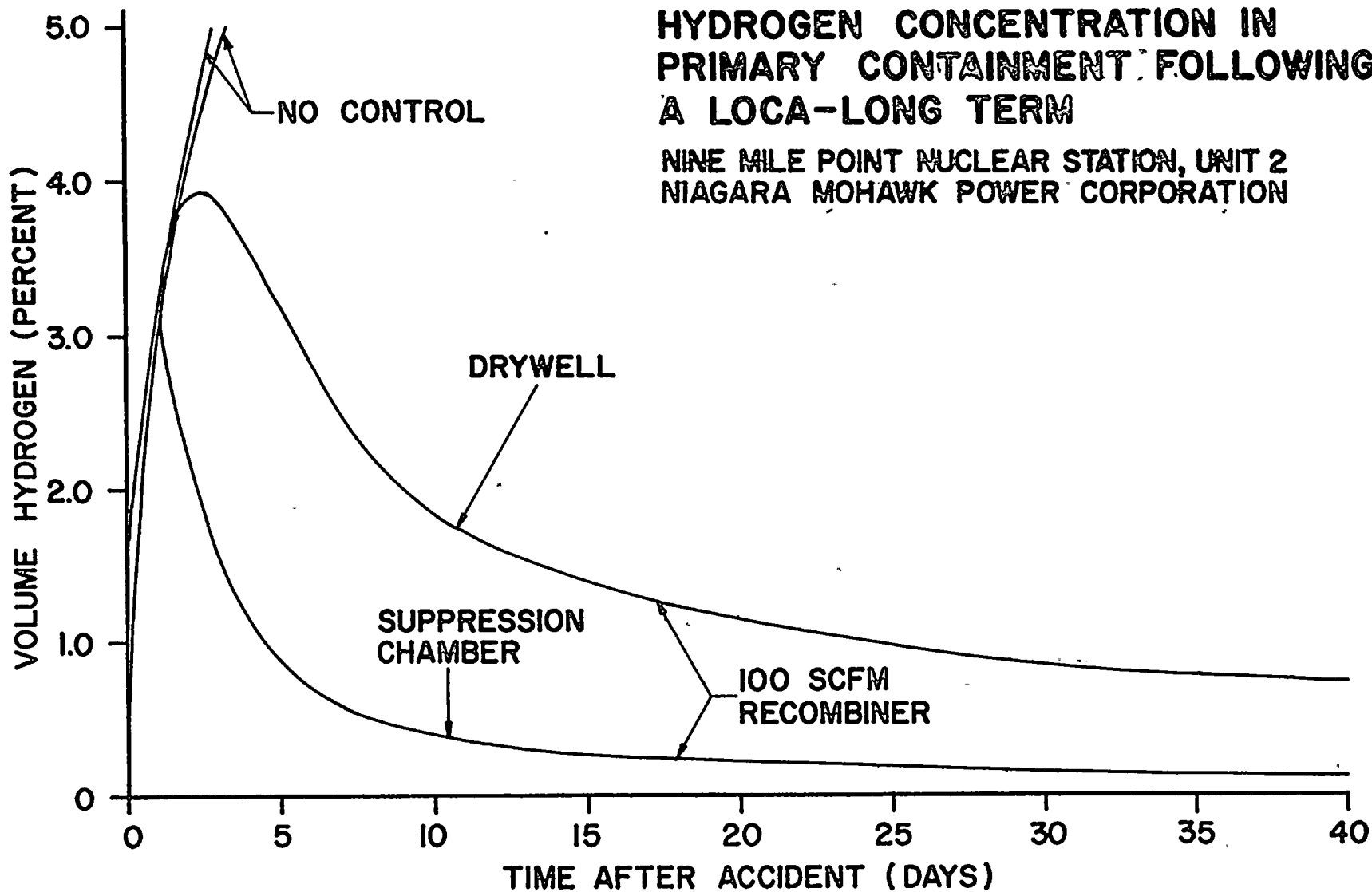
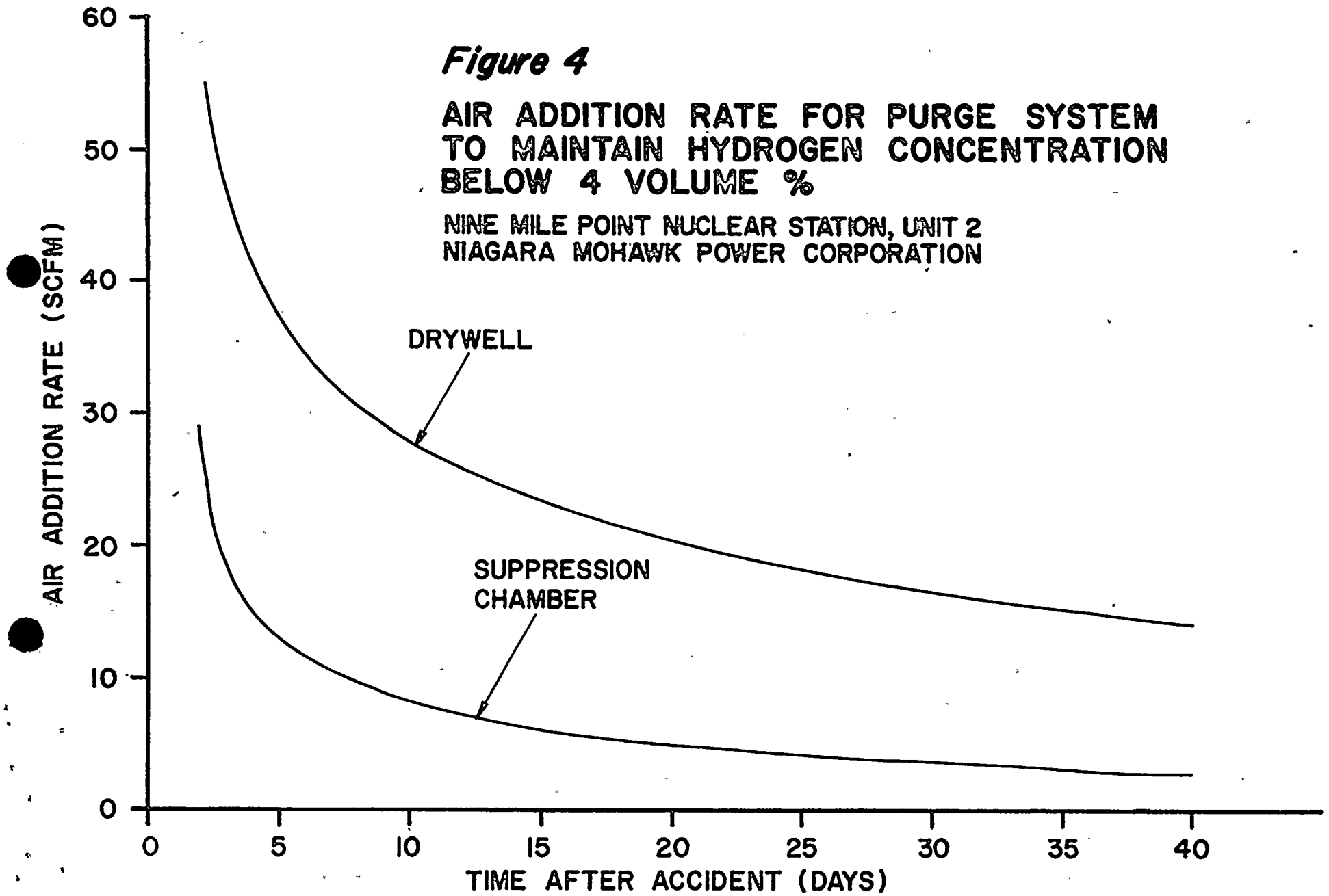


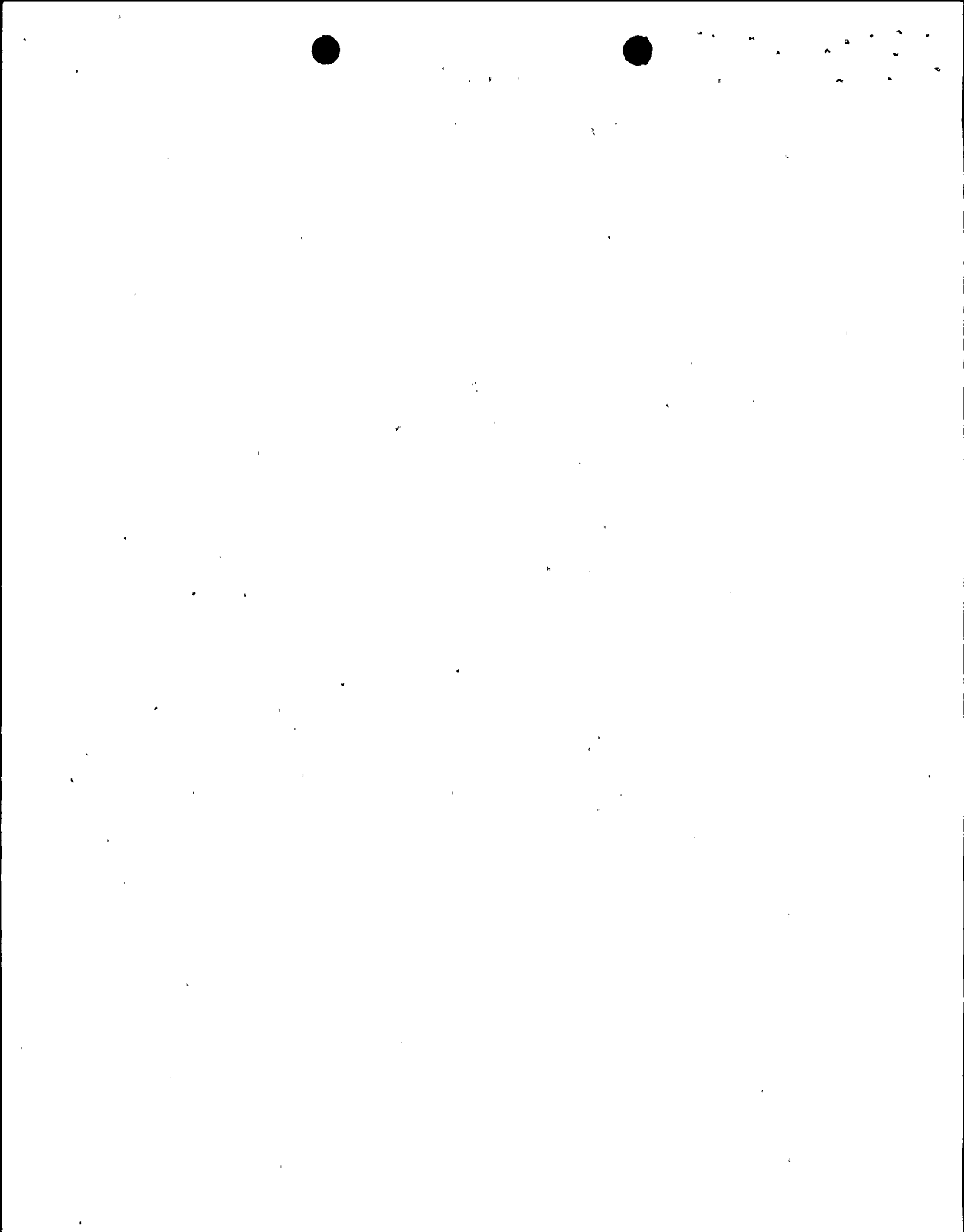


Figure 4

**AIR ADDITION RATE FOR PURGE SYSTEM
TO MAINTAIN HYDROGEN CONCENTRATION
BELOW 4 VOLUME %**

**NINE MILE POINT NUCLEAR STATION, UNIT 2
NIAGARA MOHAWK POWER CORPORATION**





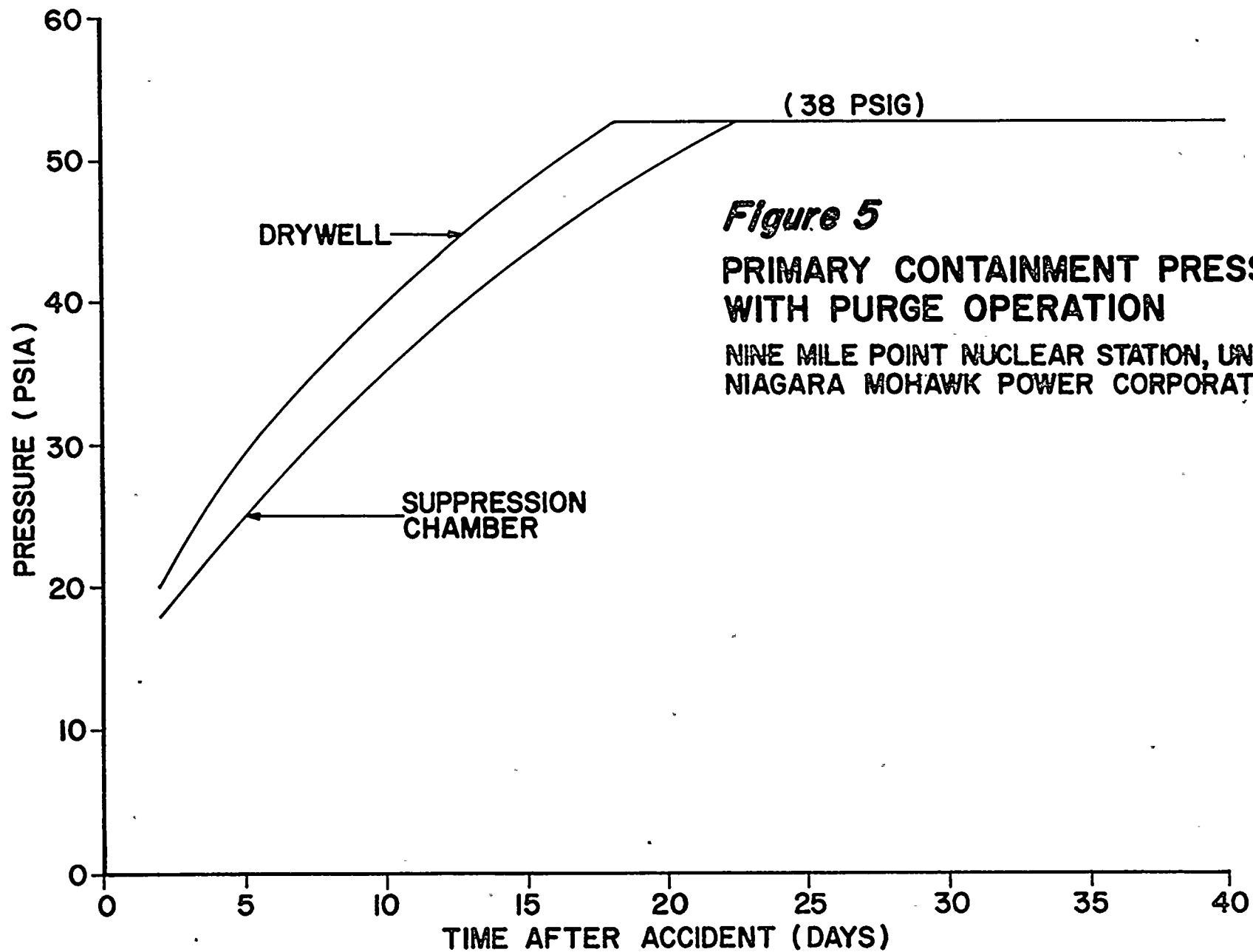


Figure 5

**PRIMARY CONTAINMENT PRESSURE
WITH PURGE OPERATION**

**NINE MILE POINT NUCLEAR STATION, UNIT 2
NIAGARA MOHAWK POWER CORPORATION**

