

Verification and Validation of Selected Fire Models for Nuclear Power Plant Applications

Supplement 1

Draft Report for Comment

U.S. Nuclear Regulatory Commission
Office of Nuclear Regulatory Research
Washington, D.C. 20555-0001

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1 ABSTRACT

2 There is a movement to introduce risk-informed and performance-based (RI/PB) analyses into
3 fire-protection engineering practice, both domestically and worldwide. This movement exists in
4 both the general fire-protection and the nuclear power-plant (NPP) fire-protection communities.
5 The U.S. Nuclear Regulatory Commission (NRC) has used risk-informed insights as part of its
6 regulatory decisionmaking since the 1990s.

7 In 2001, the National Fire Protection Association (NFPA) issued the 2001 Edition of NFPA 805,
8 "Performance-Based Standard for Fire Protection for Light-Water Reactor Electric Generating
9 Plants." In July 2004, the NRC amended its fire-protection requirements in Section 50.48, "Fire
10 Protection," of Title 10, "Energy," of the *Code of Federal Regulations* (10 CFR 50.48) to permit
11 existing reactor licensees to voluntarily adopt fire-protection requirements contained in
12 NFPA 805 as an alternative to the existing deterministic fire-protection requirements. In addition,
13 the NPP fire-protection community has been using RI/PB approaches and insights to support
14 fire-protection decisionmaking in general.

15 One key tool needed to further the use of RI/PB fire protection is the availability of verified and
16 validated (V&V) fire models that can reliably predict the consequences of fires. Section 2.4.1.2
17 of NFPA 805 requires that only fire models acceptable to the authority having jurisdiction (AHJ)
18 shall be used in fire-modeling calculations. Furthermore, Sections 2.4.1.2.2 and 2.4.1.2.3 of
19 NFPA 805 state that fire models shall only be applied within the limitations of the given model
20 and shall be verified and validated.

21 In 2007, the NRC, together with the Electric Power Research Institute (EPRI) and the National
22 Institute of Standards and Technology (NIST), conducted a research project to verify and
23 validate five fire models that have been used for NPP applications. The results of this effort
24 were documented in a seven-volume report, NUREG-1824 (EPRI 1011999), "Verification and
25 Validation of Selected Fire Models for Nuclear Power Plant Applications."

26 This supplement expands on the previous V&V effort and evaluates the latest versions of the
27 five fire models including additional test data for validation of the models. As with the previous
28 effort, the results are reported in the form of ranges of accuracies for the fire model predictions
29 and, the project was performed in accordance with the guidelines that ASTM International
30 (formerly the American Society for Testing and Materials) set forth in ASTM E1355-12,
31 "Standard Guide for Evaluating the Predictive Capability of Deterministic Fire Models" (2012).

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118		sending an e-mail request to david.stroup@nrc.gov .	

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1 EXECUTIVE SUMMARY

2 In 2007, the U.S. Nuclear Regulatory Commission (NRC) and the Electric Power Research
3 Institute (EPRI) jointly published, under a Memorandum of Understanding (MOU), NUREG-1824
4 (EPRI 1011999) “Verification and Validation of Selected Fire Models for Nuclear Power Plant
5 Applications.” This supplement builds on and furthers the original verification and validation
6 (V&V) of the five selected fire models commonly used in support of risk-informed and
7 performance-based (RI/PB) fire protection at U.S. nuclear power plants (NPPs).

8 **Background**

9 Since the 1990s, when it became the policy of the NRC to use risk-informed methods to make
10 regulatory decisions where possible, the nuclear power industry has been moving from
11 prescriptive rules and practices toward the use of risk information to supplement
12 decisionmaking. Several initiatives have furthered this transition in the area of fire protection.
13 In 2001, the National Fire Protection Association (NFPA) completed the development of the
14 2001 Edition of NFPA Standard 805, “Performance-Based Standard for Fire Protection for
15 Light-Water Reactor Electric Generating Plants.” Effective July 16, 2004, the NRC amended its
16 fire-protection requirements in Section 50.48(c) of Title 10, “Energy,” of the *Code of Federal
17 Regulations* (10 CFR 50.48(c)) to permit existing reactor licensees to voluntarily adopt
18 fire-protection requirements contained in NFPA 805 as an alternative to the existing
19 deterministic fire-protection requirements. RI/PB fire protection often relies on fire modeling for
20 determining the consequences of fires. NFPA 805 requires that the “fire models shall be verified
21 and validated,” and “only fire models that are acceptable to the Authority Having Jurisdiction
22 (AHJ) shall be used in fire modeling calculations.”

23 **Objectives**

24 The objective of this study is to quantify the predictive capabilities of five different fire models by
25 comparison with selected and available experimental data that is representative of NPP fire
26 scenarios.

27 **Approach**

28 This project team previously performed V&V studies on five selected models: (1) the NRC’s
29 NUREG-1805 “Fire Dynamics Tools” (FDT^s), (2) EPRI’s “Fire-Induced Vulnerability Evaluation”
30 (FIVE), (3) National Institute of Standards and Technology’s (NIST’s) “Consolidated Model of
31 Fire Growth and Smoke Transport” (CFAST), (4) Electricité de France’s (EdF’s) MAGIC, and
32 (5) NIST’s “Fire Dynamics Simulator” (FDS). The team based these studies on the guidelines of
33 ASTM E1355, “Standard Guide for Evaluating the Predictive Capability of Deterministic Fire
34 Models.” The scope of these V&V studies was limited to the capabilities of the selected fire
35 models and did not cover certain potential fire scenarios that fall outside the capabilities of these
36 fire models. This is documented in Volume 1 of the original NUREG-1824 (EPRI 1011999)
37 report published in 2007. This supplement uses the latest versions of each model and expands
38 on the original work.

39 **Results**

40 This study focuses mainly on model *validation* (that is, the quantification of model uncertainty).
41 Validation is a process to determine the appropriateness of the governing equations as a
42 mathematical model of the physical phenomena of interest. Typically, validation involves
43 comparing model results with experimental measurement. Differences that cannot be explained
44 in terms of numerical errors in the model or uncertainty in the measurements are attributed to

1 the assumptions and simplifications of the physical model. Model *verification* (that is, testing of
2 mathematical robustness and accuracy) is not addressed directly in this report. Rather,
3 references are provided to the models' documentation and published reports.

4 For each predicted quantity, such as plume temperature, and each model, a bias factor and
5 relative standard deviation are calculated based on comparison of the model predictions and
6 full-scale measurements. These two metrics indicate the extent to which the model under- or
7 overpredicts the quantity of interest, on average, and the extent to which its predictions are
8 scattered about the mean. The calculation of these metrics takes into consideration the
9 uncertainty in the experimental measurements.

10 **EPRI Perspective**

11 The use of fire models to support fire-protection decisionmaking requires a good understanding
12 of their limitations and predictive capabilities. This supplement to NUREG-1824 expands on the
13 previous report to provide validation of the latest versions of the fire models (FDT^s, FIVE,
14 CFAST, MAGIC, and FDS), considers additional test data to expand the validity of fire models,
15 and provides a quantifiable assessment of model accuracy. An improvement from the original
16 version replaces the qualitative color chart with a table providing quantitative estimates of
17 fire-model uncertainty. This allows the analyst to characterize fire-model uncertainty in
18 combination with user-selected input parameters. The V&V establishes acceptable use and
19 limitations of specific fire models. It is the responsibility of the analyst to justify the
20 appropriateness of each fire model for the specific applications.

21 **Keywords**

- 22 fire hazard analysis (FHA)
- 23 fire modeling
- 24 fire probabilistic risk assessment (PRA)
- 25 fire probabilistic safety assessment (PSA)
- 26 fire protection
- 27 fire safety
- 28 nuclear power plant
- 29 risk-informed performance-based (RI/PB) regulation
- 30 verification and validation (V&V)

31

1 PREFACE

2 This is the first formal expansion of a verification and validation study of five different
3 mathematical models that are commonly used in fire-hazard analyses of nuclear power plants
4 (NPPs). The original report was published as seven individual volumes in 2007. For this
5 expansion, it was decided to combine the original seven volumes into a single published volume
6 along with supplemental material that is to be released only in electronic form. This single
7 volume contains the analyses, summary information, and conclusions necessary to evaluate
8 each model for use in NPP applications. The electronic appendices contain the data summaries
9 that support the conclusions in the main report. In the original NUREG-1824 (EPRI 1011999),
10 the reader would have to refer to each volume to evaluate a specific model. The information
11 contained in the original NUREG-1824 (EPRI 1011999) remains valid for the versions of the
12 models for which the V&V documented in that report was conducted. Here are some other
13 notable differences between this supplement and the original study:

- 14 • Supplement 1 includes measurements from 16 different series of experiments,
15 compared to the 5 that were included in the original study. The number of individual
16 experiments has expanded to 340 compared to the 26 in the original study.
- 17 • Supplement 1 uses the latest versions of the modeling software available at the time of
18 the report. As newer versions of these models are released in the future, the information
19 in this report can be used as guidance in conducting V&V of these new versions. In
20 addition, some of the model authors might choose to publish revised V&V information on
21 their own as they develop new versions of their modeling software.
- 22 • Supplement 1 combines the assessment of the NRC and EPRI collections of empirical
23 correlations referred to as the Fire Dynamics Tools (FDT[®]) and the Fire Induced
24 Vulnerability Evaluation (FIVE). In the original V&V study, these tools were evaluated
25 separately, and there were several inconsistencies in the application of the various
26 calculation methods.
- 27 • Supplement 1 adds additional model output quantities to the evaluation, including
28 sprinkler and smoke-detector activation time and electrical-cable failure time.
- 29 • Supplement 1 provides a more quantifiable assessment of model accuracy. The original
30 study used a simple qualitative scheme to assess the models that proved to be difficult
31 to implement in practice. The new method allows modelers to assign meaningful
32 uncertainty bounds to model outputs.
- 33 • Supplement 1 was designed to complement the NUREG-1934 (EPRI 1023259) “Nuclear
34 Power Plant Fire Modeling Analysis Guidelines (NPP FIRE MAG).” The original V&V
35 study was published in 2007 and did not include clear guidance on the use of the results
36 of the study. The NPP FIRE MAG provides eight practical examples showing how to use
37 the results of the validation study in typical NPP fire-modeling analyses.

38

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3 support from several organizations.

4 The verification and validation (V&V) studies for the Fire Dynamics Tools (FDT^s), Consolidated
5 Model of Fire Growth and Smoke Transport (CFAST), and Fire Dynamics Simulator (FDS)
6 models were conducted in collaboration with the Fire Research Division of the U.S. Department
7 of Commerce's National Institute of Standards and Technology (NIST). Since the inception of
8 this project in 1999, the U.S. Nuclear Regulatory Commission (NRC) has collaborated with NIST
9 through an interagency memorandum of understanding (MOU) and conducted research to
10 provide the necessary technical data and tools to support the use of fire models in nuclear
11 power-plant fire-hazard analysis (FHA).

12 The following individuals or organizations contributed experimental data for use in the model
13 validation study:

- 14 • Felix Gonzalez of the Office of Nuclear Regulatory Research and Steve Nowlen of
15 Sandia National Laboratories (SNL) added more experimental data from the
16 SNL/Factory Mutual (FM) experiments. Steve Nowlen also contributed data from the
17 Cable Response to Live Fire (CAROLFIRE) program.
- 18 • David Sheppard of the Bureau of Alcohol, Tobacco, and Firearms (ATF) contributed data
19 from the ATF Corridor Experiments.
- 20 • Simo Hostikka of VTT Technical Research Centre of Finland contributed data from the
21 VTT Large Hall Experiments.
- 22 • Rob Fleury of the University of Christchurch, New Zealand, contributed radiation
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- 24 • Ulf Wickström of the SP Technical Research Institute of Sweden contributed data from
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27 contributed data from the Underwriters Laboratories (UL)/National Fire Protection
28 Research Foundation (NFPRF) experiments.
- 29 • The U.S. Navy contributed data from its high bay hangar experiments in Hawaii and
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- 31 • NIST contributed data from experiments performed by Anthony Hamins,
32 Kenneth Steckler, Richard Peacock, Robert Vettori, and Alexander Maranghides.

33

ACRONYMS AND ABBREVIATIONS

ACH	air changes per hour
AHJ	authority having jurisdiction
ANSI	American National Standards Institute
ASET	available safe egress time
AST	adiabatic surface temperature
ASTM	(no longer an abbreviation; formerly the American Society for Testing and Materials)
ATF	Bureau of Alcohol, Tobacco, Firearms and Explosives
BE	Benchmark Exercise
CAROLFIRE	Cable Response to Live Fire
CFAST	Consolidated Fire Growth and Smoke Transport Model
CFD	computational fluid dynamics
CFR	<i>Code of Federal Regulations</i>
DB	Deal and Beyler correlation
EdF	Electricité de France
EPRI	Electric Power Research Institute
FDS	Fire Dynamics Simulator
FDT ^s	Fire Dynamics Tools (NUREG-1805)
FHA	fire hazard analysis
FIVE	Fire Induced Vulnerability Evaluation Model
FM/SNL	Factory Mutual & Sandia National Laboratories
FPA	Foote, Pagni, and Alvares
HGL	hot gas layer
HRR	heat release rate
HVAC	heating, ventilation, and air conditioning
iBMB	Institut für Baustoffe, Massivbau und Brandschutz
ISO	International Organization for Standardization
LES	Large Eddy Simulation
LLNL	Lawrence Livermore National Laboratory
MCR	Main Control Room
MQH	McCaffrey, Quintiere, and Harkleroad
MOU	memorandum of understanding
NBS	National Bureau of Standards (now NIST)
NEI	Nuclear Energy Institute
NFPA	National Fire Protection Association
NFPRF	National Fire Protection Research Foundation
NIST	National Institute of Standards and Technology
NPP	nuclear power plant
NRC	U.S. Nuclear Regulatory Commission
NRR	Office of Nuclear Reactor Regulation (of the NRC)
PRA	Probabilistic Risk Assessment
PS	point source radiation model
PWR	pressurized water reactor
RES	Office of Nuclear Regulatory Research (of the NRC)
RI/PB	Risk-Informed and Performance-Based
RTI	Response Time Index

SF	solid flame radiation model
SFPE	Society of Fire Protection Engineers
SNL	Sandia National Laboratories
SP	SP Technical Research Institute of Sweden
TC	thermocouple
THIEF	Thermally Induced Electrical Failure Model
TP	thermoplastic
TS	thermoset
UL	Underwriters Laboratories
USN	United States Navy
V&V	verification and validation
VTT	VTT Technical Research Centre of Finland
WTC	World Trade Center
YT	Yamana and Tanaka smoke-filling correlation

NOMENCLATURE

Roman symbols:

A	area (m ²)
A_o	opening area (m ²)
c_p	specific heat, gas at constant pressure (kJ/kg/K)
D	fire diameter (m)
E	experimental measurement
g	acceleration of gravity (m/s ²)
H	ceiling height (m)
H_f	height of base of fire above floor (m)
H_o	opening height (m)
k	thermal conductivity (kW/m/K)
L	compartment length (m)
L_f	flame height (m)
\dot{m}	mass loss or flow rate (kg/s)
\dot{m}''	mass-loss rate per unit area (kg/s/m ²)
M	model prediction
P	probability
p	pressure (Pa)
\dot{q}''	heat flux (kW/m ²)
\dot{Q}	heat-release rate (kW)
\dot{Q}^*	fire Froude number
r	radial distance (m)
r_{cj}	ceiling jet distance (m)
t	time (s)
T	temperature (°C)
V	volume (m ³)
\dot{V}	volume flow rate (m ³ /s)
W	compartment width (m)
y	product yield (kg/kg)
Y	mass fraction (kg/kg)

Greek symbols:

δ	model bias factor
ΔH	heat of combustion (kJ/kg)
Δp	pressure difference (Pa)
φ	equivalence ratio
μ	mean
ρ	density (kg/m ³)
σ	standard deviation
$\tilde{\sigma}_E$	relative standard deviation of the experiment
$\tilde{\sigma}_M$	relative standard deviation of the model

1

INTRODUCTION

1.1 Background

In 2001, the National Fire Protection Association (NFPA) issued the first edition (the 2001 Edition) of NFPA 805, “Performance-Based Standard for Fire Protection for Light-Water Reactor Electric Generating Plants.” Effective July 16, 2004, the U.S. Nuclear Regulatory Commission (NRC) amended its fire-protection requirements in subsection 50.48(c) of Title 10, “Energy,” of the *Code of Federal Regulations* (10 CFR 50.48(c)) to permit existing reactor licensees to voluntarily adopt fire-protection requirements contained in NFPA 805 following a performance-based approach as an alternative to the existing deterministic fire-protection requirements. One important element in a performance-based approach is the estimation of fire hazard using mathematical fire models. Fire modeling is often used in constructing Fire PRAs to determine the effects of fire hazard so that the associated risk can be quantified.

As part of its fire-modeling requirements, NFPA 805 states that “fire models shall be verified and validated” (Section 2.4.1.2.3) and that “only fire models that are acceptable to the authority having jurisdiction (AHJ) shall be used in fire modeling calculations” (Section 2.4.1.2.1). This is an important requirement because the verification and validation (V&V) of fire models is intended to ensure the correctness, suitability, and overall quality of the method. Specifically, verification is the process used to determine whether a model correctly represents the developer’s conceptual description (i.e., whether it was “built” correctly), while validation is used to determine whether a model is a suitable representation of the real world and is capable of reproducing phenomena of interest (i.e., whether the correct model was “built”).

In 2007, the NRC’s Office of Nuclear Regulatory Research (RES) and the Electric Power Research Institute (EPRI) completed a collaborative project for the V&V of five select fire-modeling tools. The results of this study, which was performed under an NRC/RES-EPRI Memorandum of Understanding (MOU), were documented in NUREG-1824 (EPRI 1011999), “Verification and Validation of Selected Fire Models for Nuclear Power Plant Applications.” The National Institute of Standards and Technology (NIST) was also an important partner in developing this publication, providing extensive fire-modeling and experimentation expertise.

Subsequently, the NRC conducted a phenomena identification and ranking table (PIRT) exercise for nuclear power-plant (NPP) fire-modeling applications. A PIRT is a formal structured expert elicitation process that focuses on identifying phenomena relevant to a given analysis application (figure of merit) and then ranking the identified phenomena for both importance and current state of knowledge. The process involves the consideration of a series of specific scenarios by a panel of knowledgeable experts (the PIRT panel). For the fire-modeling PIRT, the panel considered four typical NPP fire scenarios. The scenarios included a main control room (MCR) electrical cabinet fire, a switchgear fire, a turbine building lubricating oil fire, and a cable fire in the annulus region inside containment. The potential needs associated with improving fire models for use in NPP fire-modeling applications were assessed using the PIRT results. The results of the PIRT are documented in NUREG/CR-6978, “A Phenomena Identification and Ranking Table (PIRT) Exercise for Nuclear Power Plant Fire Modeling Applications,” published in 2008.

INTRODUCTION

1 In 2012, RES and EPRI completed a collaborative project to develop a set of guidelines to
2 assist users of fire models in applying the technology to the NPP environment. NUREG-1934
3 (EPRI 1023259), “Nuclear Power Plant Fire Modeling Analysis Guidelines (NPP FIRE MAG),”
4 presents a step-by-step process for using fire modeling in NPP applications. The process
5 described in the guide addresses most of the technical elements relevant to fire-modeling
6 analysis, such as the selection and definition of fire scenarios and the determination and
7 implementation of input values, sensitivity analysis, uncertainty quantification, and
8 documentation. In addition, requirements associated with fire-modeling analyses and analytical
9 fire-modeling tools are addressed through generic guidance, recommended best practices, and
10 example applications. The results from the original NUREG-1824 (EPRI 1011999) were used
11 and expanded to demonstrate the implications of fire model V&V on NPP applications.

12 This report expands on the previous V&V effort and builds on the lessons learned from the PIRT
13 and the NPP FIRE MAG. The latest versions of the five fire models are used in this V&V
14 exercise. Additional fire test data has been incorporated into this supplement to expand the
15 range of validity of the fire models. In the original NUREG-1824, (EPRI 1011999) two suites of
16 algebraic models, FDT^s and FIVE Revision 1, were selected for V&V. This supplement focuses
17 on the validation of the individual models within the two suites. As a result of work on
18 NUREG-1934 (EPRI 1023259), the qualitative color chart used in the original NUREG-1824
19 (EPRI 1011999) report has been superseded with a quantitative assessment of fire-model
20 uncertainty. The use of these quantitative estimates of the uncertainties associated with each
21 model’s predictions represents a significant step forward in the use of fire modeling for NPP
22 applications.

23 **1.2 Objectives**

24 The purpose of this supplement is to expand the evaluation of the predictive capabilities of
25 certain fire models for applications specific to NPPs. The use of fire models in NPP applications
26 has been previously documented in NUREG-1934 (EPRI 1023259). Section 2.4.1.2 of
27 NFPA 805 states that only fire models acceptable to the AHJ shall be used in fire-modeling
28 calculations. Further, Sections 2.4.1.2.2 and 2.4.1.2.3 of NFPA 805 state that fire models shall
29 only be applied within the limitations of the given fire model and shall be verified and validated.
30 Thus, V&V is necessary to establish acceptable uses and limitations of fire models. In addition,
31 analysts need to justify the appropriateness of fire models for specific applications.

32 Verification and validation of a calculation method are intended to ensure the correctness and
33 suitability of the method. Verification is the process to determine that a model correctly
34 represents the developer’s conceptual description. It is used to decide whether the model was
35 “built” correctly. Validation is the process to determine that a model is a suitable representation
36 of the real world and is capable of reproducing phenomena of interest. It is used to decide
37 whether the right model was “built.”

38 **1.3 Scope**

39 Numerous fire models have been developed and maintained by various organizations to predict
40 fire-generated conditions. This study selects the following five of these fire models commonly
41 used for NPP Fire Hazard Analysis (FHA), which represent a wide range of capabilities and
42 mathematical and computational sophistication:

- 43 1. NRC’s Fire Dynamics Tools (FDT^s version 1805.1)
- 44 2. EPRI’s Fire-Induced Vulnerability Evaluation (FIVE- Rev2)

- 1 3. National Institute of Standards and Technology's (NIST's) Consolidated Model of Fire
- 2 Growth and Smoke Transport (CFAST Version 6.3.1)
- 3 4. Electricité de France's (EdF) MAGIC (Version 4.1.3)
- 4 5. NIST's Fire Dynamics Simulator (FDS Version 6.0.0)

5 These particular models were chosen based on the fact that most of them have been used to
6 calculate fire conditions in NPP fire-protection applications, or were developed by stakeholders
7 within the nuclear industry for NPP fire-protection applications. Details of the models are
8 included in Chapter 4.

9 **1.4 Approach**

10 This report follows the guidelines of ASTM E1355, "Evaluating the Predictive Capability of
11 Deterministic Fire Models" (2012). This standard identifies the necessary steps in the evaluation
12 of predictive fire models. Another useful reference is the Society of Fire Protection Engineers'
13 "Guidelines for Substantiating a Fire Model for a Given Application" (2011).

14 **Chapter 2: Define typical NPP fire scenarios and predicted quantities of interest.** This list
15 of fire scenarios is intended to be a reflection of the wide range of fire scenarios found in NPPs
16 (i.e., the scope of scenarios for which models would need validation). However, some aspects
17 of these scenarios cannot be predicted with available models or do not have any available
18 experimental data to support a quantitative model evaluation.

19 **Chapter 3: Select experimental data to perform the quantitative validation.** The selected
20 experiments contain a variety of elements typical of the fire scenarios in NPPs. In addition,
21 these experiments are well documented, the data is publicly available, the major parameters
22 (such as the heat-release rate of the fire) are well characterized, and the measurement
23 laboratories are recognized for their experience in the area of fire measurements.

24 **Chapter 4: Select and describe the fire models for which an evaluation can be conducted.**
25 To be consistent with ASTM E1355, the description of the selected fire models includes a
26 review of their theoretical basis and fundamental assumptions and an assessment of their
27 mathematical and numerical robustness.

28 **Chapter 5: Conduct the quantitative validation study for each fire-modeling tool.** The
29 quantitative validation studies are conducted by comparing experimental measurements with
30 model predictions of quantities deemed of importance in NPP fire scenarios. For each selected
31 output quantity, the difference between the models and the experiments is expressed in the
32 form of a bias factor and a relative standard deviation. Examples of using these uncertainty
33 metrics are given in NUREG-1934 (EPRI 1023259).

34 **Chapter 6: Conclusions.** This section presents the conclusions from this V&V study.

35 **Chapter 7: References.** This section contains the list of references used in this report.

36 In addition, several electronic files are available as supporting material. These additional files
37 include four reports that present the results of comparisons between the model calculations and
38 individual experiments (empirical correlations, CFAST, MAGIC, and FDS); the input files for the
39 model comparisons; and the versions of the FDT^s, CFAST, and FDS used for this study. FIVE
40 and MAGIC are only available through EPRI (www.epri.com).

41

INTRODUCTION

- 1 The electronic files are included on the CD accompanying this report and are also available for
- 2 download from the following web site:¹
- 3 <http://www.nrc.gov/reading-rm/doc-collections/nuregs/staff/>
- 4

¹ During the public comment period, the electronic files may be obtained by sending an e-mail request to david.stroup@nrc.gov.

2

IDENTIFICATION OF FIRE-MODELING CAPABILITIES

To conduct the verification and validation (V&V) study in accordance with ASTM E1355, it is necessary to identify the fire scenarios of interest against which the model will be evaluated. Specifically, the identification of fire scenarios provides a broad definition for the scope of the V&V study. The term “fire scenario” as used in fire-modeling applications for the commercial nuclear industry is a broad term capturing various elements characterizing a fire event. These elements include ignition, fire growth, fire propagation to secondary combustibles, detection and suppression features and activities, and damage to plant equipment. Fire models for these applications are used to quantify or predict some of these elements. Fire growth, propagation to secondary combustibles, and damage to plant equipment are the elements often evaluated using fire-modeling tools. This chapter expands on such elements with the purpose of identifying specific fire phenomena predicted by the selected fire models that will form the basis for the V&V study.

The fire phenomena forming the basis for the V&V analysis are selected based on significant research conducted over the last ten years by NRC and EPRI identifying and modeling typical nuclear power plant (NPP) fire scenarios. Specifically:

- Volume 1 of NUREG-1824 (EPRI 1011999) presented a list of fire scenarios that are routinely evaluated, and
- NUREG-1934 (EPRI 1023259) provides detailed examples of how the fire scenarios identified in NUREG-1824 (EPRI 1011999) can be analyzed using the fire models within the scope of this V&V study.

The material in this chapter is based on the research published in the two references listed above. It is not the intent of this V&V study to reproduce or expand the library of fire scenarios already developed and in use by the industry. Instead, this chapter focuses on describing and justifying the specific fire-induced phenomena (i.e., fire dynamics) within these fire scenarios that are the subjects of the V&V study.

2.1 Library of Nuclear Power-Plant Fire Scenarios

The concept of “the library of nuclear power-plant fire scenarios” is used for defining the scope of the V&V study. The library of scenarios consists of a list of fire events that are routinely postulated and analyzed for commercial NPP applications using a combination of modeling tools. Within this library of scenarios, specific fire-induced phenomena are predicted by fire models. This section summarizes the fire scenarios included in the library as introduction to the description of the specific fire-induced phenomena that are the subjects of the V&V. A brief summary of the process for selecting such scenarios is presented first.

IDENTIFICATION OF FIRE-MODELING CAPABILITIES

1 **2.1.1 Fire-Scenario Selection Process**

2 The process for selecting the fire scenarios included in the library was based on the following
3 activities:

- 4 • Review the range of possible configurations that contribute to the postulated fire
5 scenarios in the U.S. commercial nuclear industry. The review focused on parameters
6 considered important in the definition of fire scenarios.
- 7 • Identification of potentially risk-significant fire scenarios through review of recent
8 experience in developing probabilistic risk assessments for fires, and
- 9 • Examination of past industry experience with fire modeling in support of regulatory
10 applications to help define these fire scenarios.

11 As a result of these activities, the library of fire scenarios analyzed in NUREG-1934
12 (EPRI 1023259) was developed. These scenarios are summarized next for completeness
13 purposes. Detailed fire-modeling analyses for these scenarios are available in NUREG-1934
14 (EPRI 1023259).

15 **2.1.2 Summary of Nuclear Power-Plant Fire Scenarios**

16 This section provides a summary of the selected NPP fire scenarios. The scenarios are:

17 **Fire Scenarios in Switchgear Rooms:** Switchgear rooms house key power-distribution
18 equipment to support the plant. Consequently, it is one of the plant locations where detailed
19 fire-modeling analysis is conducted in support of the requirements of a fire-protection program.
20 Typical ignition sources in switchgear rooms include electrical cabinets, transformers and
21 transient fires. Fire modeling is often used for determining plume temperatures, flame radiation
22 conditions, and hot gas layer temperatures in the room. Fire-modeling analysis is also used for
23 determining the time at which specific cables will be damaged or ignited and the heat-release
24 rate generated by fire propagating through cable trays.

25 **Fire Scenarios in Cable-Spreading Rooms:** Cable-spreading rooms (CSRs) are another
26 critical location in commercial NPPs because they often contain redundant instrumentation and
27 control circuits needed for plant operation. These rooms generally contain high concentrations
28 of electrical cable (in cable trays and/or conduits), where fire propagation in open cable trays
29 can be an important aspect of fire modeling. Some plants also have areas called cable shafts,
30 cable tunnels, or cable lofts, which present similar challenges. These areas might also contain
31 significant amounts of cables in trays or conduits and might contain redundant circuits. Typical
32 ignition sources in these rooms include low-voltage electrical cabinets and transient fires. Fire
33 modeling is often used for determining plume temperatures, flame radiation conditions, and hot
34 gas layer temperatures in the room. Fire-modeling analysis is also used for determining the time
35 at which specific cables will be damaged or ignited and the heat-release rate generated by fire
36 propagating through cable trays.

37 **Fire Scenarios in Main Control Rooms:** The main control room (MCR) contains redundant
38 instrumentation and control circuits that are critical to plant control and operation. Analyses of
39 fires in MCRs pose unique challenges, including timing of fire detection, smoke generation,
40 migration, and habitability (including visibility and concentration of species); fire propagation
41 within very large panels; and fire propagation between panels. It should also be noted that some
42 plants have areas (i.e., a relay room, auxiliary equipment room, or remote shutdown panel) that
43 are similar to control rooms in that they contain redundant instrumentation and control circuits

IDENTIFICATION OF FIRE-MODELING CAPABILITIES

1 that are critical to plant control and safe shutdown. However, such areas are not constantly
2 manned as MCRs are and might instead be equipped with automatic suppression systems.
3 A fire in this location might lead to a situation in which the reactor cannot be controlled from the
4 MCR because of damage to the instrumentation and control circuits and must be shut down
5 from an alternative or dedicated location. The source of a fire in this scenario might be, for
6 example, a control cabinet. The size of the fire will depend on the type and amount of cables
7 within the cabinet, as well as on cabinet ventilation and detection and suppression activities in
8 the constantly manned control room. MCRs are usually equipped with smoke purge systems
9 that can be accounted for in fire-modeling analyses. Important targets are adjacent control
10 cabinets exposed to radiant heat flux or flame impingement. Another important aspect of MCR
11 fire scenarios is the habitability conditions in the room as the fire progresses. Habitability
12 conditions refer to smoke concentration (which affects visibility and toxicity), heat flux from the
13 hot gas layer, and room temperature. These conditions are important for determining when
14 operators might need to leave the MCR as a result of relatively high temperatures or low
15 visibility.

16 **Fire Scenarios in Pump Rooms:** This location represents areas in a plant where a relatively
17 large fire is possible in a small enclosure. However, not all pump rooms are small, because
18 relatively large pumps can be found in large open areas such as turbine building elevations. The
19 source of a fire in this scenario might be ignition of an oil pool spilled from a pump. The size of
20 the fire will depend on the type and amount of oil spilled, as well as the area and depth of the
21 pool itself. The growth of this fire typically will be fast, and depending on the size of the room,
22 the fire could possibly generate flashover conditions that might challenge integrity of the walls
23 and ceiling. Targets of interest in these scenarios might be the walls and ceiling of the
24 enclosure, which are fire barriers, as well as any other safety-related equipment and cables
25 located in the room or area. These targets might be exposed to direct flame impingement, flame
26 radiation or plumes, ceiling jets, or hot gas layer conditions.

27 **Fire Scenarios in Turbine Buildings:** A turbine building is usually a very large open multi-level
28 enclosure², in which the top level is commonly referred to as the turbine operating deck. A fire
29 scenario just below the turbine deck was selected to examine large (e.g., turbine lube oil) or
30 small (e.g., transient or panel) fires in large enclosures with high ceilings. The scenario can
31 apply to buildings with one or more turbines. The source of a fire in this scenario might be
32 ignition of an oil pool spilled from one of the turbines. The size of the fire will depend on the type
33 and amount of oil spilled, as well as the area and depth of the pool itself. The growth of this fire
34 will be fast. Other sources of fire in the turbine building could be electrical fires
35 (e.g., high-energy arcing faults), transformer or switchgear fires, and hydrogen fires. Turbine
36 buildings are often naturally ventilated, with many open shafts (e.g., open equipment hatches),
37 doors, and windows. There might also be mechanical ventilation using roof-mounted exhaust
38 fans and/or mechanical supply. Targets of interest in these scenarios might be structural steel
39 members and fire barriers, as well as any other safety-related equipment and cables located in
40 the area and exposed to the fire. Fire conditions affecting the targets might include direct flame
41 impingement, fire plume conditions, or flame radiation.

42 **Fire Scenarios in Multi-Compartment Configurations:** Most NPPs have areas with multiple
43 compartments that open into a common space or corridor. Fire scenarios in these areas involve

² Some NPPs (typically in warmer climates) do not have a turbine building; instead, the main turbine is open to the elements.

IDENTIFICATION OF FIRE-MODELING CAPABILITIES

1 both natural and mechanical ventilation and the propagation of smoke over considerable
2 distances. Targets of interest are typically safety-related equipment and cables located in the
3 corridor outside the room where the fire originates or in an adjacent room.

4 **Fire Scenarios in Multi-Level Buildings:** Most NPPs have areas with multiple levels
5 connected by open hatches or staircases. A typical example is the turbine building. The source
6 of a fire in a turbine building might be ignition of an oil pool spilled from an oil tank located under
7 one of the turbine generators. The heat and smoke created will flow through the mezzanine
8 opening between levels. Ventilation is typically natural through openings on the upper level.
9 There might also be mechanical ventilation using roof-mounted exhaust fans and/or mechanical
10 supply.

11 **Fire Scenarios in Containment Buildings:** The containment building in a PWR plant is unique
12 because of its cylindrical geometry, high domed ceiling, and large volume. It has internal
13 air-recirculation systems with cooling units. No fresh air is added to the containment building
14 during normal operation. The target of interest in this scenario is an elevated cable tray located
15 outside the fire plume. These targets might be exposed to direct flame impingement, flame
16 radiation or plumes, ceiling jets, or hot gas layer conditions.

17 **Fire Scenarios in Battery Rooms:** Battery rooms are typically small concrete enclosures
18 containing large banks of batteries. These rooms are kept closed and are typically free of
19 transient combustibles and fixed ignition sources other than the batteries themselves. EPRI's
20 Fire Events Database suggests two types of scenarios: (1) explosion of the battery cells during
21 the charging phase of the battery and (2) fires in battery terminals as a result of defective or
22 unsecured terminals. Rooms are usually mechanically ventilated. The targets of interest in this
23 scenario are nearby cables and batteries. These targets might be exposed to direct flame
24 impingement, flame radiation or plumes, ceiling jets, or hot gas layer conditions.

25 **Diesel Generator Room:** Diesel generator rooms house the standby diesel generator (SBDG)
26 and associated electrical cabinets. This scenario consists of a fuel oil fire near the diesel
27 generator. The size of the fire will depend on the type and amount of fuel oil spilled, as well as
28 the area and depth of the pool itself. The growth of this fire will be fast. The ventilation
29 conditions in the room will be mechanical ventilation with leakage around closed doors. Targets
30 of interest in these scenarios might be cables located in the room exposed to HGL
31 temperatures. These targets might be exposed to direct flame impingement, flame radiation or
32 plumes, ceiling jets, or hot gas layer conditions.

33 **Computer or Relay Room:** Computer rooms are typically located in close proximity to the
34 MRCs in NPPs. In addition to computers and other office equipment, some computer rooms
35 might house control cabinets or banks of relay panels. The ignition source for this scenario is a
36 transient combustible fire, namely a computer workstation. The size of the fire will depend on
37 the amount and type of materials involved. The ventilation conditions will be mechanical
38 ventilation. The targets of interest might be control cabinets or banks of relay panels or cables
39 above the fire. These targets might be exposed to direct flame impingement, flame radiation or
40 plumes, ceiling jets, or hot gas layer conditions.

41 **Outdoors:** Outdoor fire scenarios can involve large oil-filled transformers or hydrogen tanks;
42 such fires can affect or propagate to nearby equipment. Nearby equipment can include other
43 transformers, other electrical equipment, turbine building walls, etc. Considering that fires will be
44 outdoors, fire conditions that could affect targets include flame radiation and exposure to fire
45 plumes. In the case of transformers, fires can be attributable to oil leaks or spills or electrical
46 faults. Consequences will depend on the type of fire analyzed (i.e., a "regular" fire vs. an
47 explosion).

2.2 Fire-Induced Phenomena for Verification and Validation

A comprehensive review of the fire phenomena (i.e., fire dynamics) developing in the scenarios described in the previous section was performed to identify capabilities within the fire models that should be verified and validated. This comprehensive review also considered the available experimental data that could support the validation process. The result of the review is a list of fire-induced phenomena that (1) can be predicted by the modeling tools within the scope of this study, (2) yield fire-modeling results that can be compared with experimental data, and (3) are routinely used in commercial nuclear plant fire-modeling applications. Consequently, the V&V study presented in this report does not cover all the predictive capabilities of each model and focused only on the identified capabilities. The specific fire-modeling capabilities subjected to the verification and validation process include:

Temperature of the hot gas layer (HGL): The HGL temperature is particularly important in NPP fire scenarios because it is an indicator of overhead target damage (e.g., to cable trays) away from the ignition source. The empirical correlations and zone models typically predict an average HGL temperature, while CFD models predict the local gas temperature in each computational grid cell.

Height of the hot gas layer: The height of the HGL is also important in NPP fire scenarios because it indicates whether a given target is immersed in high-temperature gases. HGL height is a direct output of a two-zone model and can be calculated from local gas temperatures predicted by a CFD model. The empirical correlations can predict the HGL height only for very simple compartment geometries.

Temperature of the ceiling jet: The ceiling jet is the shallow layer of hot gases that spreads radially below the ceiling as the fire plume flow impinges on it. This layer of hot gases has a distinct temperature that is higher than the temperature associated with the HGL. The ceiling-jet temperature is important for modeling NPP fire scenarios in which targets are located just below the ceiling and for determining activation of heat-detection devices. A variety of empirical correlations predict the ceiling-jet temperature and are embedded in the zone models. CFD models compute the ceiling-jet temperature directly.

Plume temperature: The fire plume is the buoyant flow of hot gases rising from the base of the fire. The fire plume transports hot gases into the HGL. Its temperature is greater than the ceiling jet and HGL temperature. It is particularly important in NPP fires because of the numerous postulated scenarios that involve targets directly above a potential fire. A variety of empirical correlations predict the plume temperature and are embedded in the zone models. CFD models compute the plume temperature directly.

Flame height: The height of the flame is important in those NPP fire scenarios in which targets are located close to the ignition source. Some of these scenarios subject the target to flame temperatures because the distance between the target and the ignition source is less than the predicted flame height. A typical example would be cable trays above an electrical cabinet. A variety of empirical correlations predict the flame height and are embedded in the zone models. CFD models compute the flame height directly as a consequence of the combustion model.

Heat flux to targets: Thermal radiation and convection are important modes of heat transfer in fire events. The models included in this study address heat flux with various levels of sophistication, from simply estimating flame radiation from a point source to solving the full radiation-transport equation. The empirical models include simple estimates of flame radiation from a point or cylindrical source. Zone models include these same estimates, as well as

IDENTIFICATION OF FIRE-MODELING CAPABILITIES

1 radiation exchange between hot and cold layers and surfaces. CFD models solve the
2 radiation-transport equation that predicts the gains and losses of thermal radiation from each
3 individual gas- and solid-phase grid cell.

4 **Heat flux to surfaces (walls, floors, and ceilings):** Surface heat flux refers to the incident or
5 net heat fluxes received by room surfaces such as walls, floors, or ceilings. As an example of
6 the use of these predictions, consider the evaluation of heat fluxes from room surfaces and the
7 hot gas layer to the floor in a control-room fire for determining whether operators need to
8 abandon the room. For the purposes of the V&V, these model outputs are considered
9 separately to determine whether the zone and CFD models have any particular strengths or
10 weaknesses depending on the particular surface considered. The empirical correlations do not
11 address heat flux to the various compartment surfaces.

12 **Target temperature:** Target temperature refers to the surface temperature of specific items
13 within the computational domain. The calculation of target temperature is perhaps the most
14 common objective of fire-modeling analyses. A typical nuclear power-plant application is the
15 calculation of cable temperatures caused by fire-generated conditions. The zone and CFD
16 models calculate the surface temperature of the target as a function of time and consider the
17 heat conducted into the target material.

18 **Cable failure time:** Cable failure time is one of the most important fire-modeling outputs
19 because it is often compared with the time to start detection and suppression activities. It
20 specifically refers to the time it takes a fire to increase the surface or internal temperature of a
21 cable to its damage or ignition temperature. Zone and CFD models predict the temperature and
22 heat-flux levels surrounding a cable. The models use such predictions for estimating surface
23 and internal cable temperatures. For calculating the surface or internal temperature of the cable,
24 hand calculations, such as the model for the Thermally Induced Electrical Failure (THIEF) of
25 cables (Supplement 1 to NUREG-1805), treat the gas temperature surrounding the cables as an
26 input to the model.

27 **Surface (wall, floor, and ceiling) temperature:** Surface temperature refers to the increase in
28 the temperature of room surfaces such as walls, floors, or ceilings caused by fire-generated
29 conditions. As an example of the use of these predictions, consider the evaluation of heat fluxes
30 from room surfaces and the hot gas layer to the floor in a control-room fire for determining
31 whether operators need to abandon the room. For the purposes of the V&V, these outputs are
32 considered separately to determine whether the zone or CFD models have any particular
33 strengths or weaknesses depending on the particular surface considered. The empirical
34 correlations do not address the temperatures of the various compartment surfaces.

35 **Smoke concentration:** The smoke concentration can be an important attribute in NPP fire
36 scenarios that involve rooms where operators might need to perform actions during a fire. This
37 attribute specifically refers to soot concentration, which affects visibility. It can also be used for
38 determining smoke-detector activation. Zone and CFD models calculate smoke concentration
39 as a function of time. While the empirical correlation spreadsheets can provide visibility
40 estimates, these calculation methods were not evaluated in this V&V study.

41 **Oxygen concentration:** Oxygen concentration is an indicator of a fire becoming
42 underventilated, a pre-cursor to flashover. The zone models calculate the oxygen concentration
43 in the upper and lower layers; CFD models calculate the oxygen concentration in each grid cell.
44 Some of the empirical correlations contain oxygen-concentration calculations embedded in
45 individual spreadsheets. These embedded calculations were not considered in this V&V study.

IDENTIFICATION OF FIRE-MODELING CAPABILITIES

1 **Room pressure:** Room pressure is a rarely used quantity in NPP fire modeling. It might be
2 important when it contributes to smoke migration to adjacent compartments or modeling
3 mechanically ventilated spaces. Zone and CFD models calculate room pressure as they solve
4 energy and mass balance equations for individual compartments. Empirical correlations only
5 apply in the simplest of room geometries.

6 **Sprinkler activation time:** Sprinkler activation time is an important fire-modeling output
7 because it is often compared with the cable or target damage time. It specifically refers to the
8 time it takes a fire to increase the temperature of the activation element³ in a sprinkler or
9 heat-detector device. Zone and CFD models predict the temperature and heat flux levels
10 surrounding the sprinkler and calculate its thermal response considering its “response-time
11 index” (RTI). Hand calculations operate in a similar way but consider only ceiling jet conditions
12 heating the sprinkler or heat-detector device.

13 **Smoke-detector activation time:** Smoke-detector activation is often the trigger for suppression
14 activities, either by automatic systems or a fire brigade, in the analysis of fire scenarios.
15 Smoke-detector activation time specifically refers to the time it takes a fire to generate the
16 smoke-concentration conditions necessary to activate the smoke-detection device. Zone and
17 CFD models predict the temperature levels surrounding the smoke detector and determine
18 whether they have exceeded an activation temperature serving as a surrogate for smoke
19 concentration. Hand calculations operate in a similar way.

20 The fire-modeling capabilities listed above are the bases for the validation study. Fire
21 experiments properly designed and instrumented for collecting data associated with the fire
22 phenomena predicted by the models provide the measured values used for comparison with the
23 model predictions. The following chapters describe the selected experiments, the technical
24 approach for comparing experimental results with model predictions, and the validation results.

25

³ For sprinklers, the activation element is typically a fusible link or glass bulb. For heat detectors, the activating element is typically a eutectic metal or bimetal strip.

3

EXPERIMENTAL DATA

This chapter describes the experiments selected for the validation study. Section 3.1 presents a brief description of the experiments. Section 3.2 defines the overall range of experimental parameters. Section 3.3 discusses the experimental uncertainty.

3.1 Description of Experiments

High-quality experimental data are essential to performing a sound validation study. Every effort has been taken to ensure that only reputable high-quality data were used in this project. The experiments described below were conducted at a variety of test labs over the past 30 years. The respective test reports contain different amounts of information relevant to modeling. Where appropriate, modeling assumptions have been provided in cases in which the test report is lacking in information. The criteria for selecting a particular set of experimental measurements are as follows:

- The experiments are representative of the NPP fire scenarios described in Chapter 2.1.2.
- The test report and data are of sufficient detail, are well documented, and are publicly available.
- The HRR of the fire is well characterized, meaning that its relative standard uncertainty is less than 10 percent.
- The experiments have well-defined initial and boundary conditions.
- The experimental test series includes multiple experiments, preferably replicates.

All of the 26 experiments included in the 2007 edition of NUREG-1824 (EPRI 1011999) are included below. While data from Benchmark Exercises #4 and #5 of the International Collaborative Fire Model Project (ICFMP) (Röwekamp, 2008) has been retained for consistency, this supplement uses the data only for HGL temperature and depth comparisons. Supplement 1 to NUREG-1824 (EPRI 3002002182) now includes new data sets from multiple and replicate experiments that span and expand the parameter space covered by the original benchmark exercises.

3.1.1 ATF Corridor Experiments

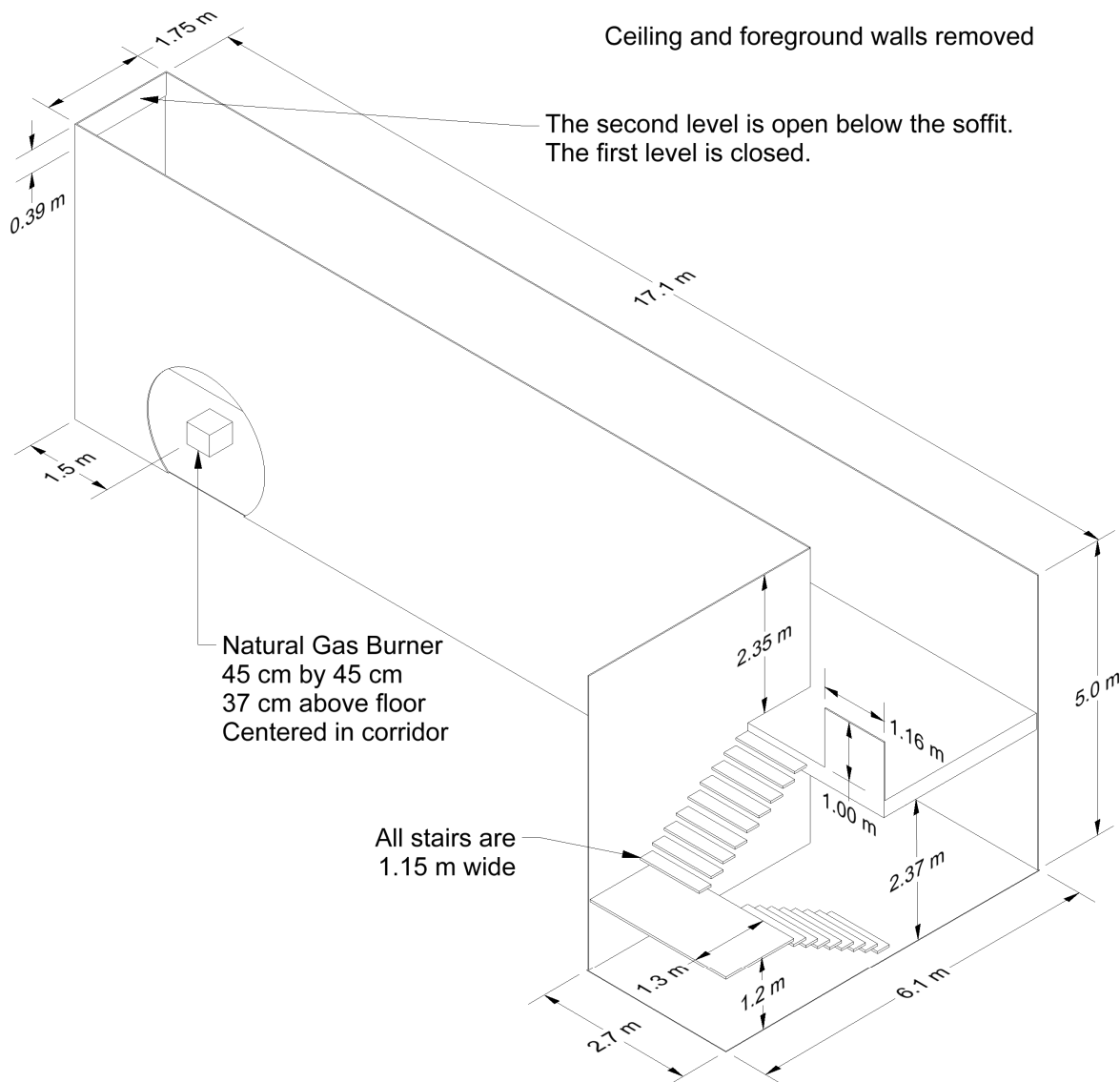
A series of eighteen experiments (six sets of three replicates) were conducted in a two-story structure with long hallways and a connecting stairway at the Bureau of Alcohol, Tobacco, Firearms, and Explosives' (ATF's) Fire Research Laboratory in Ammendale, Maryland, in 2008 (Sheppard and Klein, 2009).

Geometry: A diagram of the test structure is displayed in Figure 3-1. Two 17 m long (55.8 ft long) hallways were connected by a stairway consisting of two staircases and an intermediate landing. The first-floor hallway was closed to the outside. The end of the second-floor hallway was open with a 0.4 m (1.3 ft) soffit near the ceiling. The two staircases were separated by a 0.4 m wide (1.3 ft wide) gap.

Wall Linings: The walls and ceilings of the test structure were constructed of 1.2 cm (0.5 in) gypsum wallboard. The flooring throughout the structure, including the stairwell landing floor, consisted of one layer of 1.3-cm-thick (0.5-in-thick) cement board on one layer of 1.9 cm thick

EXPERIMENTAL DATA

- 1 (0.75 in thick) plywood supported by wood joists. The stairs were constructed of 2.5 cm thick
2 (1 in thick) clear pine lumber.
- 3 Heat Release Rate: A natural gas diffusion burner was used for the fire. Six sets of three
4 replicate experiments were performed. The HRRs were 50 kW, 100 kW, 240 kW, 250 kW,
5 500 kW, and a combination of HRRs ramped up and down. The burner surface was horizontal
6 and square, measured 0.45 m (1.5 ft) on each side, was 0.37 m (1.3 ft) above the floor, and was
7 filled with gravel. The burner was located near the end of the first floor away from the stairs.
8 There is no reported radiative fraction; thus, a value of 0.25 was chosen, which would be typical
9 of a relatively large methane fire.
- 10 Measurements: Vertical arrays of bare-bead thermocouples and bidirectional probes were
11 positioned at various locations in the corridors; one also extended the height of the stairwell.
- 12 Please see the report "Burn Tests in Two Story Structure with Hallways" (Sheppard and
13 Klein, 2009) for details concerning the ATF Corridor Experiments.



1
2 **Figure 3-1. Drawing of the ATF Corridor Experiment.**

3 **3.1.2 CAROLFIRE – Cable Response to Live Fire**

4 CAROLFIRE was a project sponsored by the U.S. Nuclear Regulatory Commission to study the
5 fire-induced thermal response and functional behavior of electrical cables (NUREG/CR-6931,
6 Vol. 3). The primary objective of CAROLFIRE was to characterize the various modes of
7 electrical failure (e.g., hot shorts and shorts to ground) within bundles of power, control, and
8 instrument cables. A secondary objective of the project was to test a simple model to predict
9 thermally induced electrical failure of cables. The measurements were conducted at Sandia
10 National Laboratories (SNL) and are described in Volume 2 of the CAROLFIRE test report
11 (NUREG/CR-6931, 2007). The experiments were conducted within a heated cylindrical
12 enclosure where single and bundled cables were exposed to various heat fluxes and the
13 electrical failure modes recorded. The experiments used for the validation study do not involve a
14 fire.

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1 The THIEF model is described in Volume 3 of the CAROLFIRE test report. It is basically the
2 solution of the one-dimensional heat-conduction equation within a homogenous non-reacting
3 cylinder with a constant thermal conductivity and specific heat.

4 Please see the three-volume report "Cable Response to Live Fire (CAROLFIRE)"
5 (NUREG/CR-6931, 2007) for details concerning the CAROLFIRE – Cable Response to Live Fire
6 Experiments.

7 **3.1.3 Fleury Heat-Flux Measurements**

8 Rob Fleury, a student at the University of Canterbury in Christchurch, New Zealand, measured
9 the heat flux from a variety of propane fires (Fleury, 2010). The objective of the work was to
10 evaluate a variety of empirical heat-flux calculation methods.

11 Heat Release Rate: The fires were fueled by propane burners with dimensions of 0.3 m (1 ft) by
12 0.3 m (1 ft) (1:1 burner), 0.6 m (2 ft) by 0.3 m (1 ft) (2:1 burner), and 0.9 m (3 ft) by 0.3 m (1 ft)
13 (3:1 burner). The heat-release rates were set to 100 kW, 150 kW, 200 kW, 250 kW, and
14 300 kW. Fifteen experiments were conducted. The radiative fraction of the fires was assumed to
15 be 0.35.

16 Measurements: Heat-flux gauges were mounted on moveable dollies that were placed in front
17 of, and to the side of, the burners. The gauges were mounted at heights of 0 m, 0.5 m (1.6 ft),
18 1.0 m (3.3 ft), and 1.5 m (4.9 ft) relative to the top edge of the burner. The horizontal distance
19 from the center of the burner varied between 0.5 m (1.6 ft) and 2 m (6.6 ft).

20 Please see the report "Evaluation of Thermal Radiation Models for Fire Spread between
21 Objects" (Fleury, 2010) for details concerning the Fleury Heat Flux Measurements.

22 **3.1.4 FM/SNL Experiments**

23 The Factory Mutual & Sandia National Laboratories (FM/SNL) series consisted of
24 25 compartment-fire experiments conducted in 1985 for the NRC by Factory Mutual Research
25 Corporation (FMRC), under the direction of SNL (NUREG/CR-4681). The primary purpose of
26 these experiments was to provide data with which to validate computer models for various types
27 of compartments typical of nuclear power plants. Six of the experiments were conducted with a
28 full-scale control-room mockup in place. Parameters varied during the experiments included fire
29 intensity, enclosure ventilation rate, and fire location. The current validation study uses data
30 from nineteen experiments (Tests 1 through 17, 21, and 22) in which propylene gas burners,
31 heptane pools, and methanol pools were used as fire sources.

32 Geometry: The experiments were conducted in an enclosure measuring approximately 18 m
33 (59 ft) long by 12 m (39 ft) wide by 6 m (19.7 ft) high, constructed at the FMRC fire test facility in
34 Rhode Island. A drawing is included in Figure 3-2.

35 Heat Release Rate: The peak heat-release rates varied from 500 kW to 2000 kW following a
36 4-minute t -squared growth profile. The test report contains detailed time histories of Tests 4, 5,
37 and 21. The time histories of the other fires are assumed to be similar. The radiative fraction
38 was not measured during the experiment, but in this study it is assumed to equal 0.35, which is
39 typical for hydrocarbon fuels that generate visible smoke.

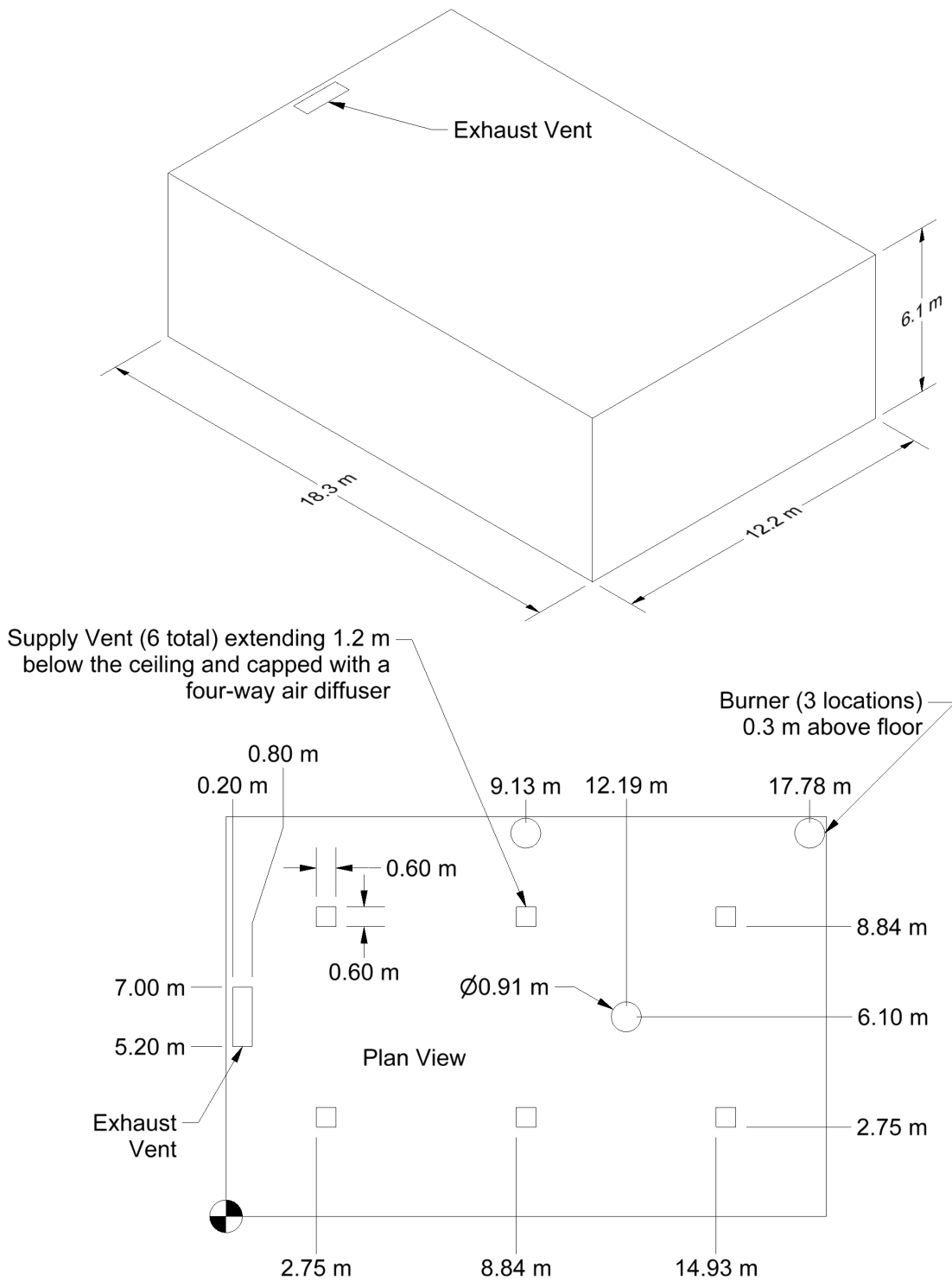
40 Ventilation: All of the experiments included forced ventilation to simulate typical power-plant
41 conditions. The rate varied from 1 to 10 air changes per hour.

1 Measurements: Four types of measurements were conducted during the FM/SNL test series
2 that are used in the current model evaluation study, including the HGL temperature and depth
3 and the ceiling jet and plume temperatures. Aspirated thermocouples (TCs) were used to make
4 all of the temperature measurements. Generally, aspirated TC measurements are preferable to
5 bare-bead TC measurements, because systematic radiative exchange measurement error is
6 reduced. Data from all of the vertical TC trees were used when reducing the HGL height and
7 temperature. For the majority of the tests, the TC data from different locations in the
8 compartment was weighted evenly when computing the HGL temperature and depth.

9 Please see the reports “An Experimental Investigation of Internally Ignited Fires in Nuclear
10 Power Plant Control Cabinets” (Volume 2 of NUREG/CR-4527, 1988) and “Enclosure
11 Environment Characterization Testing for the Base Line Validation of Computer Fire Simulation
12 Codes” (NUREG/CR-4681, 1987) for details concerning the FM/SNL Experiments.

13

EXPERIMENTAL DATA



1
 2 **Figure 3-2. Drawing of the FM/SNL compartment.**

3.1.5 iBMB Experiments

Experiments were conducted at the Institut für Baustoffe, Massivbau und Brandschutz (iBMB) of Braunschweig University of Technology in Germany. The results from two sets of experiments were contributed to the International Collaborative Fire Model Project (ICFMP) (Röwekamp, 2008) and documented in reports by Klein-Heßling (2006) and Riese (2006). These experiments, referred to as Benchmark Exercises (BEs) #4 and #5, involved relatively large fires in a relatively small concrete enclosure. Despite concerns expressed in the 2007 edition of NUREG-1824 (EPRI 1011999) regarding the use of this data, one experiment from each series was used in the original report because they span an important parameter space for fire-model validation. While new datasets have now been added to Supplement 1 to NUREG-1824 (EPRI 3002002182) that cover the range of test parameters spanned by the iBMB data, these two experiments are being retained in this report for consistency. However, only the HGL temperature and depth measurements are being used in the current study.

Geometry: BE #4 was conducted in a 3.6 m (12 ft) by 3.6 m (12 ft) by 5.7 m (19 ft) concrete enclosure (Figure 3-3). The compartment was configured slightly differently for BE #5 (Figure 3-4). Its height was 5.6 m (18.4 ft) and its doorway was also of a different height.

Heat Release Rate: The fuel source for BE #4 was a 1 m (3.3 ft) by 1 m (3.3 ft) square pan filled with Type A-1 jet fuel. The test report (Klein-Heßling, 2006) indicates the thermophysical properties of the jet fuel were similar to dodecane. The peak HRR for this test was estimated from mass-loss measurements to be approximately 3500 kW. As indicated in the test report, several difficulties were encountered in measuring the mass-loss rate, including data loss attributed to an instrument malfunction and significant fluctuations in the measured mass-loss rate. Because of the measurement issues and because the combustion efficiency was not well characterized, the HRR was assigned a relatively large expanded uncertainty of ± 25 percent in the original 2007 edition of NUREG-1824 (EPRI 1011999).

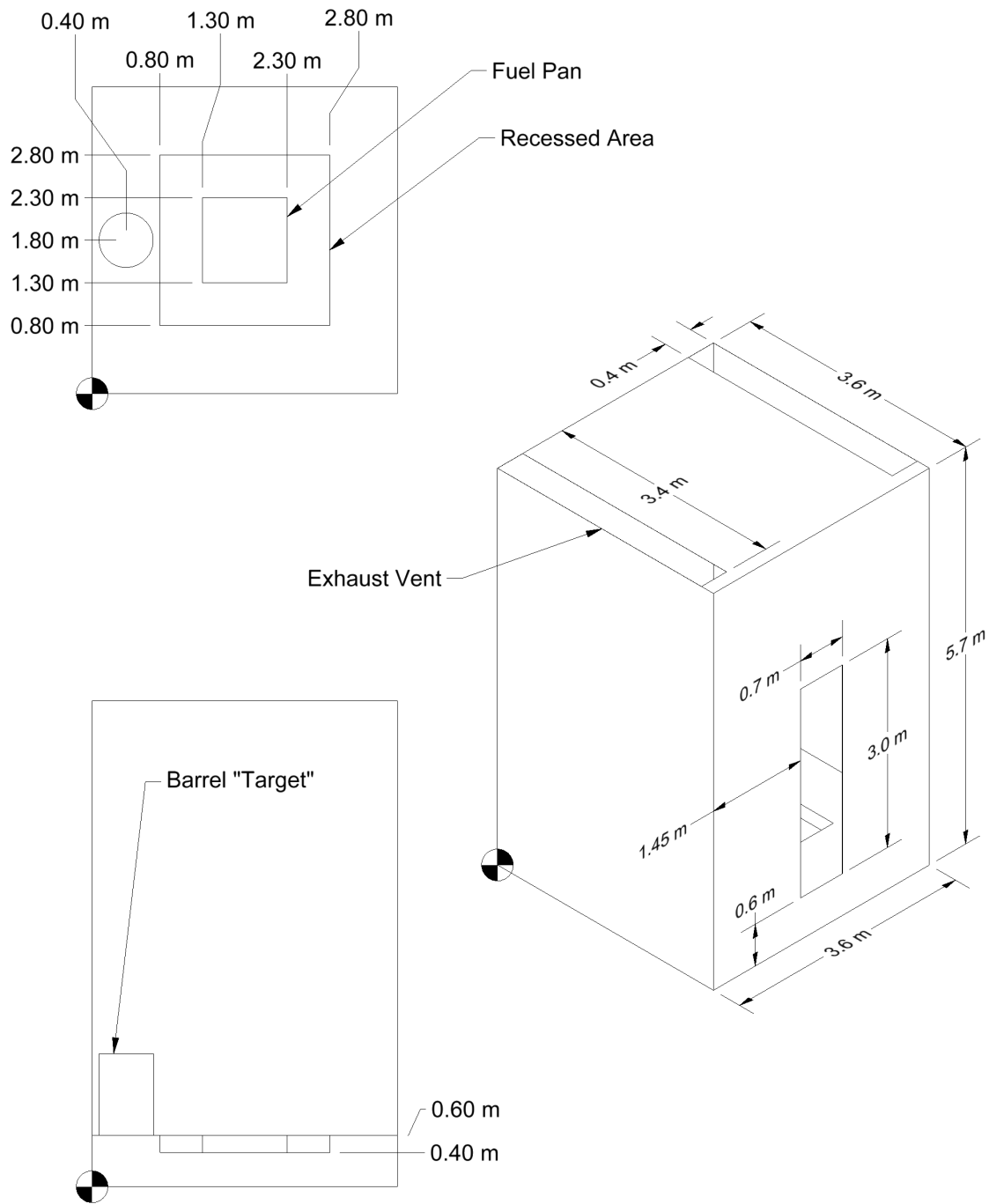
BE #5 consisted of realistically routed cables in a concrete enclosure. In one of the experiments, the compartment was preheated for 20 minutes with a 0.5 m² (5.4 ft²) pan containing ethyl alcohol. After preheating, a propane gas burner was used to ignite the cables. The HRR was measured using oxygen-consumption calorimetry. Only the preheating stage of this single experiment was used in the 2007 edition of NUREG-1824 (EPRI 1011999) because the burning rate of the cables was erratic and its HRR was difficult to measure.

The radiative fraction of the jet fuel in BE #4 was taken as 0.35, similar to that of other smoky hydrocarbons. The radiative fraction for the relatively smoke-free ethanol pool fire in BE #5 was taken as 0.20.

Ventilation: For BE #4, the original test specification called for the ventilation system within the test compartment to be closed. However, measurements made during the experiments suggest that the ventilation system was not closed, and the test report (Klein-Heßling, 2006) indicates that the volume flow rate through the ventilation system was as high as 2.25 m³/s (5,000 ft³/min) during the experiment. According to additional information provided by one of the authors of the test report, this measurement was made at a single point within an exhaust duct with dimensions 0.4 m (1.3 ft) wide and 0.8 m (2.6 ft) high. Given the complexity of the air movement within the compartment and the exhaust system, the single volumetric flow measurement is highly uncertain.

Measurements: Vertical arrays of bare-bead thermocouples were positioned within the enclosure for determining HGL temperature and depth.

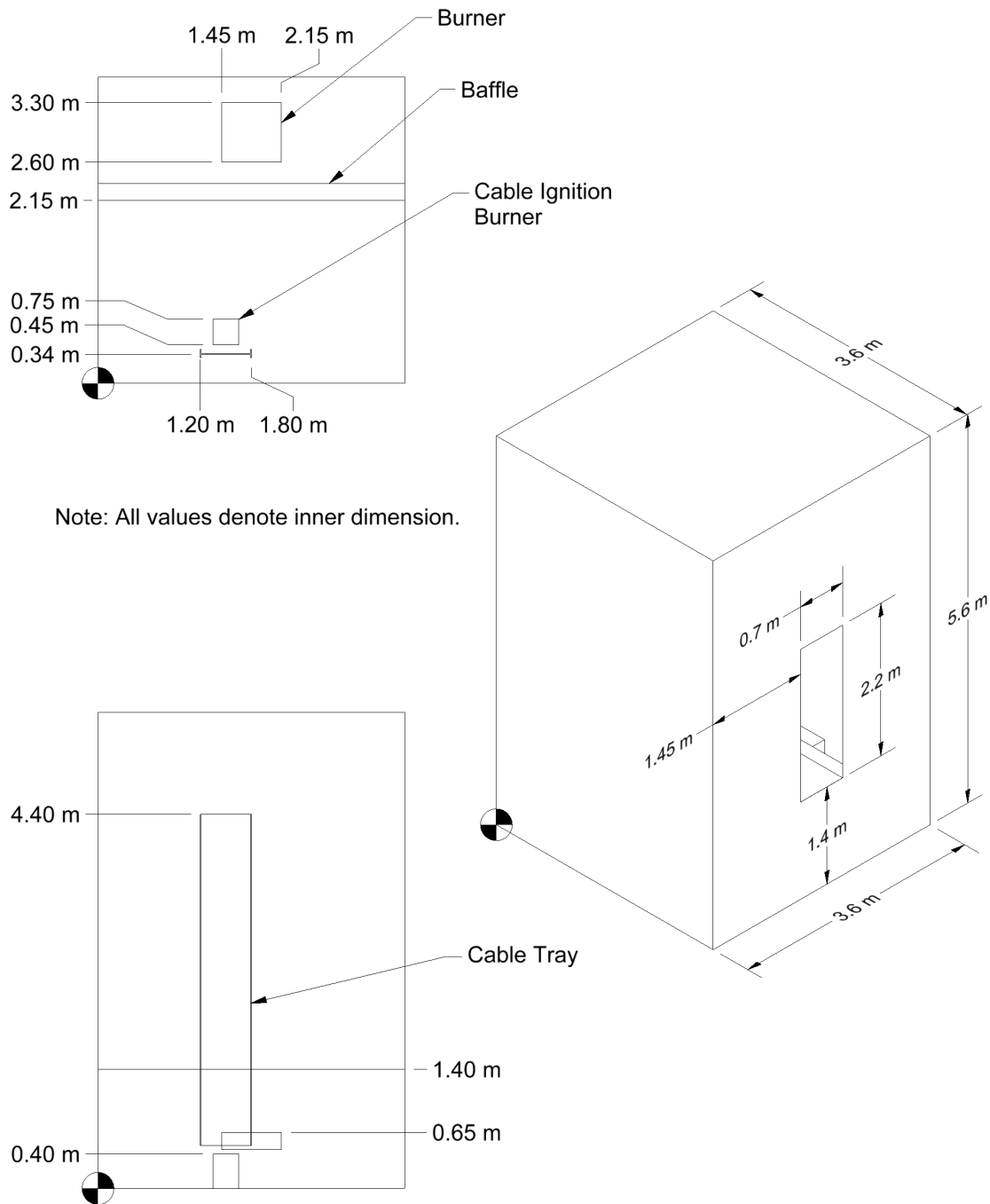
EXPERIMENTAL DATA



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2 **Figure 3-3. Drawing of the iBMB compartment used in Benchmark Exercise #4.**

3



1
 2 **Figure 3-4. Drawing of the iBMB compartment used in Benchmark Exercise #5.**
 3

EXPERIMENTAL DATA

1 **3.1.6 LLNL Enclosure Experiments**

2 Sixty-four experiments were conducted by Lawrence Livermore National Laboratory (LLNL)
3 in 1986 to study the effects of ventilation on enclosure fires (Foote, 1987).

4 Geometry: The test enclosure was 6 m (19.7 ft) long, 4 m (13.1 ft) wide, and 4.5 m (14.8 ft) high
5 (Figure 3-5). For some of the experiments, the compartment was divided into a 3 m high
6 (9.8 ft high) lower space and a 1.5 m high (4.9 ft high) upper plenum space.

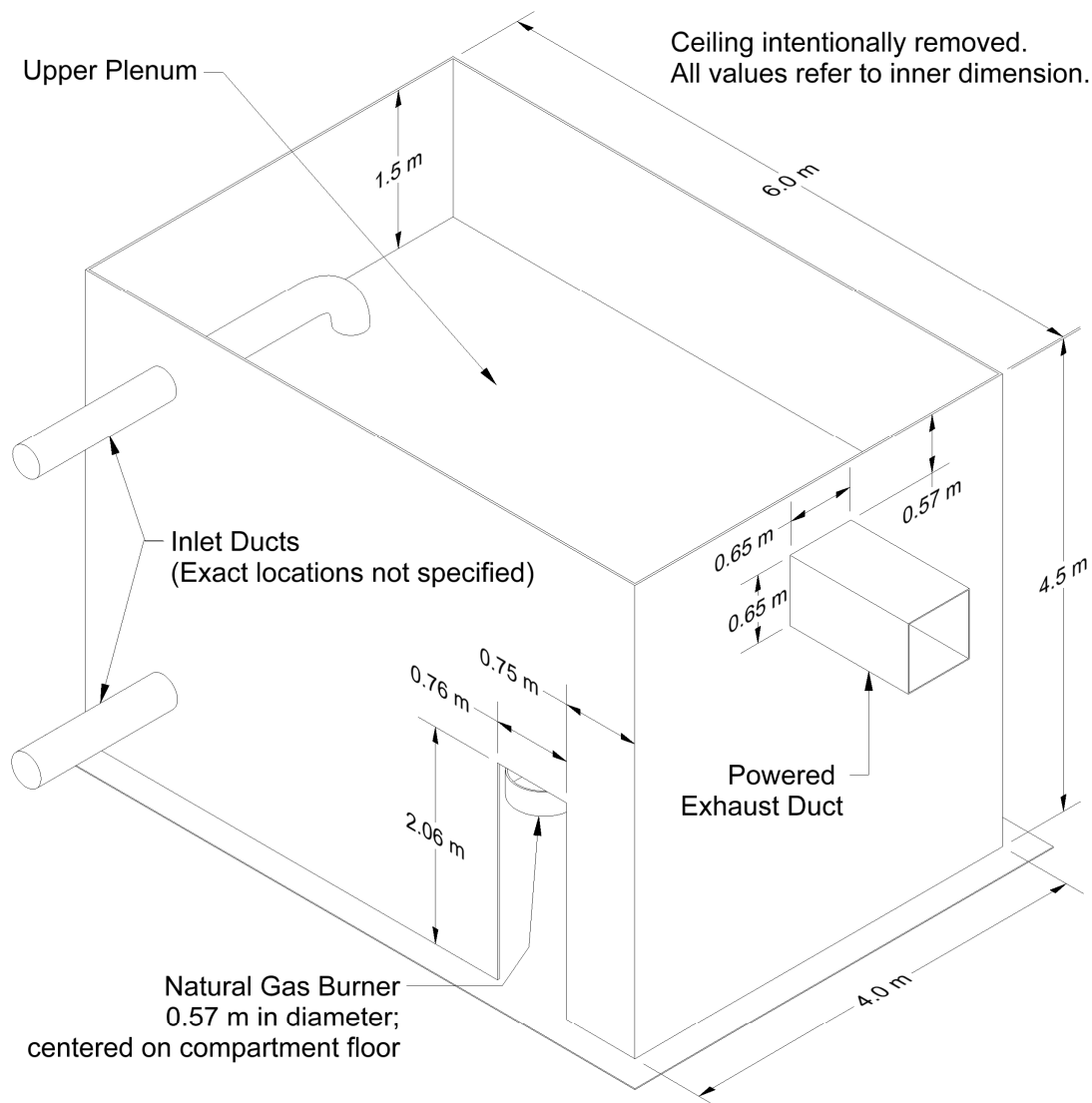
7 Heat Release Rate: A methane burner was placed directly in the center of the enclosure. For
8 most of the tests the burner was placed on the floor. The fires varied in size from 50 kW to
9 400 kW. The burner was 0.57 m (4.9 ft) in diameter and 0.23 m (0.75 ft) in height. The radiative
10 fraction was assumed to be 0.20, typical of low-soot-producing methane fires.

11 Ventilation: The door was closed and sealed for most tests and air was pulled through the space
12 at rates varying from 100 g/s to 500 g/s. Makeup air was provided through one of two ducts: one
13 supplying the lower compartment and one supplying the upper plenum space. In the numerical
14 simulations, an effective inlet area was calculated based on the reported volume flow rate and
15 pressure drop before the fire was ignited.

16 Measurements: Two vertical arrays of fifteen thermocouples each were positioned along the
17 length of the compartment to the left and right of the fire. Five of the fifteen TCs were located in
18 the upper plenum. In addition, pressure measurements were made in the upper and lower
19 spaces.

20 Please see the report "An Experimental Investigation of Internally Ignited Fires in Nuclear Power
21 Plant Control Cabinets" (Foote, 1987) for details concerning the LLNL Enclosure Experiments.

22



1
2 **Figure 3-5. Drawing of LLNL compartment.**

3 **3.1.7 NBS Multi-Room Experiments**

4 The National Bureau of Standards (NBS), now called the National Institute of Standards and
5 Technology (NIST), conducted an NBS Multi-Room series (consisting of 45 fire experiments and
6 representing 9 different sets of conditions) in a three-room suite. The experiments were
7 conducted in 1985 and are described in detail by Peacock et al. (1988). For the current study,
8 only three of the experiments have been used.

9 Geometry: The enclosure consisted of two relatively small rooms connected by a relatively long
10 corridor, as shown in Figure 3-6.

11 Heat Release Rate: A natural gas burner was located against the rear wall of one of the small
12 compartments. Fire tests of 100 kW, 300 kW, and 500 kW were conducted. For the current
13 study, only three 100-kW fire experiments have been used, including Test 100A from Set 1,

EXPERIMENTAL DATA

1 Test 100O from Set 2, and Test 100Z from Set 4. These tests were selected because they had
2 been used in prior validation studies and because they had the steadiest values of measured
3 heat-release rate during the steady-burn period. In the two tests for which the door was open,
4 the HRR during the steady-burn period measured by oxygen-consumption calorimetry was
5 110 kW. It was assumed that the closed-door test (Test 100O) had the same HRR as the
6 open-door tests.

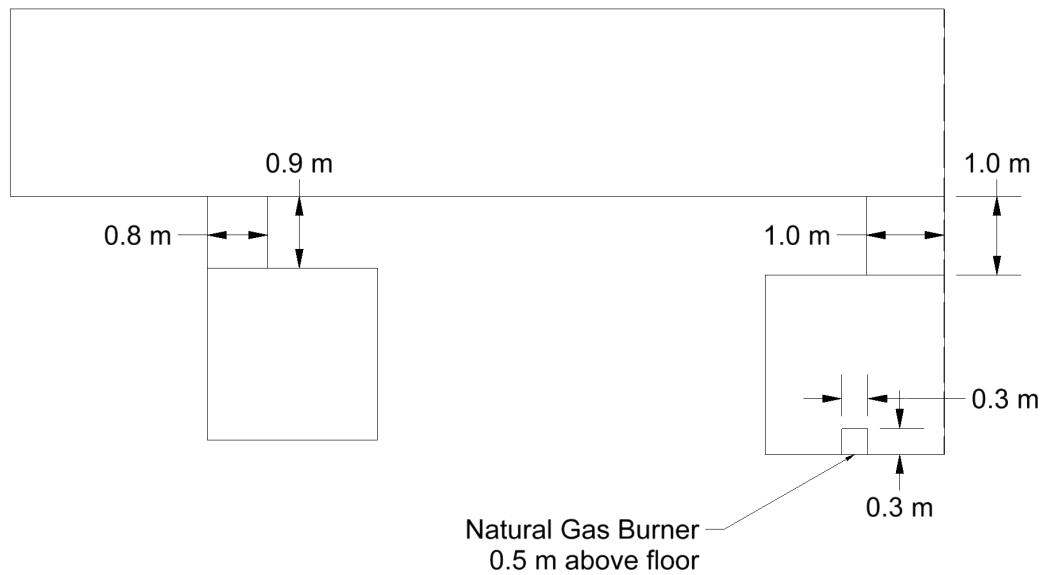
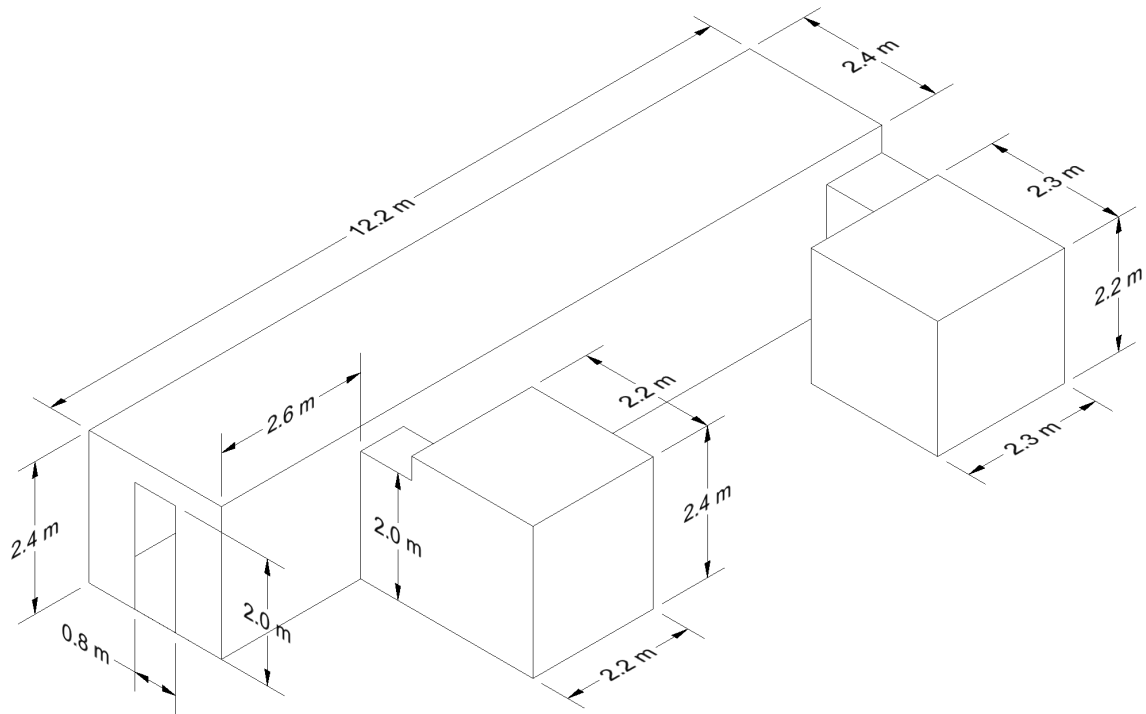
7 Radiative Fraction: Natural gas was used as the fuel in Test 100A. In Tests 100O and 100Z,
8 acetylene was added to the natural gas to increase the smoke yield, and as a consequence the
9 radiative fraction increased. The radiative fraction of natural gas has been studied previously,
10 whereas the radiative fraction of the acetylene/natural gas mixture has not been studied. The
11 radiative fraction for the natural gas fire was assigned a value of 0.20, whereas a value of 0.30
12 was assigned for the natural gas/acetylene fires.

13 Measurements: Only two types of measurements conducted during the NBS test series were
14 used in the evaluation considered here, because there was less confidence in the other
15 measurements. The measurements considered here were the HGL temperature and depth, for
16 which bare-bead TCs were used to make these measurements. Single-point measurements of
17 temperature within the burn room were not used in the evaluation of plume or ceiling jet
18 algorithms. This is because the geometry was not consistent in either case with the
19 assumptions used in the model algorithms of plumes or jets. Specifically, the burner was
20 mounted against a wall, and the room width-to-height ratio was less than that assumed by the
21 various ceiling-jet correlations.

22 Please see the report "An Experimental Data Set for the Accuracy Assessment of Room Fire
23 Models" (Peacock et al., 1988) for details concerning the NBS Multi-Room Experiments.

24

EXPERIMENTAL DATA



1
2 **Figure 3-6. Drawing of NBS Multi-Room Experiment.**

EXPERIMENTAL DATA

1 **3.1.8 NIST/NRC Experiments**

2 These experiments, sponsored by the U.S. NRC and conducted at NIST, consisted of
3 15 large-scale experiments performed in 2003. All 15 tests were included in the validation study.
4 The experiments are documented in NUREG/CR-6905 (Hamins, 2006). Ventilation conditions,
5 fire size, and fire location were varied. Numerous measurements (approximately 350 per test)
6 were made, including gas and surface temperatures, heat fluxes, and gas velocities.

7 Geometry: The test room had dimensions of 21.7 m (71.2 ft) deep by 7.1 m (23.3 ft) wide by
8 3.8 m (12.5 ft) high, designed to represent a compartment in a nuclear power plant containing
9 power and control cables (Figure 3-7). The room had one door and a mechanical air-injection
10 and -extraction system.

11 Wall Linings: The walls and ceiling were covered with two layers of calcium silicate boards, each
12 layer 1.25 cm (0.5 in) thick. The floor was covered with one layer of gypsum board on top of a
13 layer of plywood. Thermophysical and optical properties of the calcium silicate and other
14 materials used in the compartment are given in the test report (Hamins, 2006).

15 Heat Release Rate: The fire sizes ranged from 350 kW to 2.2 MW. A single nozzle was used to
16 spray liquid hydrocarbon fuels onto a 1 m by 2 m (3.3 ft by 6.6 ft) fire pan that was about 10 cm
17 (4 in) deep. The test plan originally called for the use of two nozzles to provide the fuel spray.
18 Experimental observation suggested that the HRR was steadier using a single nozzle. In
19 addition, it was observed that the actual extent of the liquid pool was well approximated by a
20 1 m (3.3 ft) circle in the center of the pan. For safety reasons, the fuel flow was terminated when
21 the lower layer's oxygen concentration dropped to approximately 15 percent by volume. The
22 fuel used in 14 of the tests was heptane, while toluene was used for one test (Test 17).

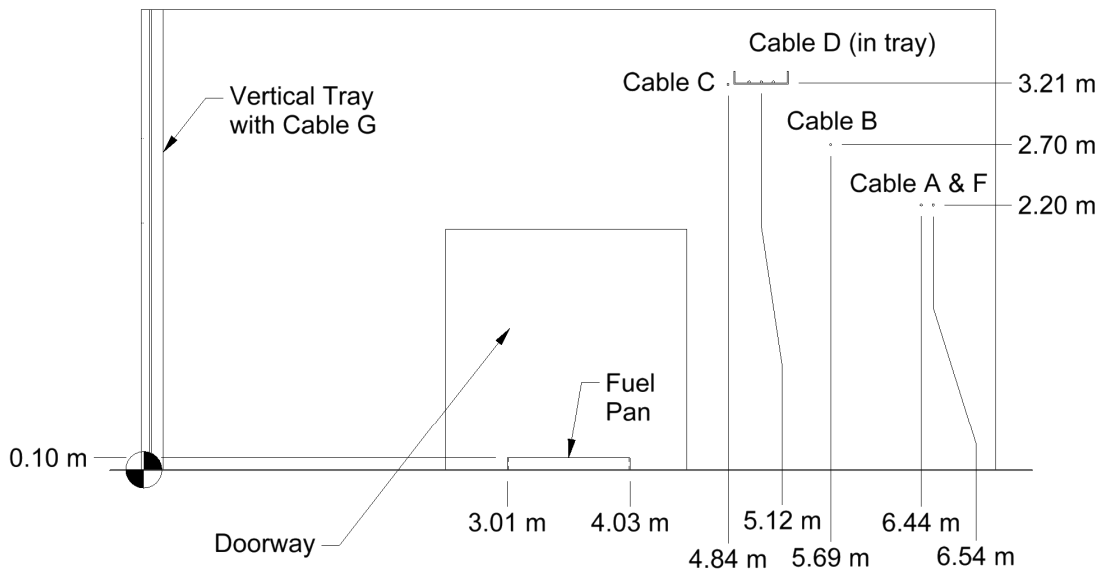
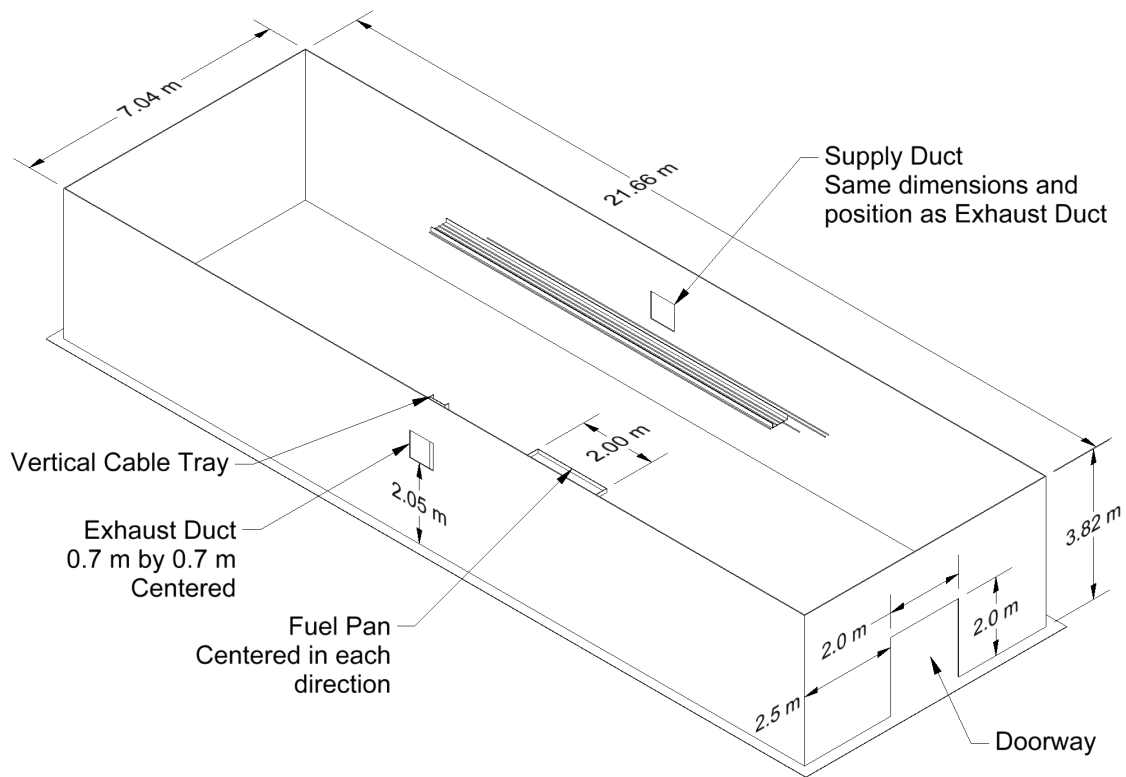
23 Radiative Fraction: The values of radiative fraction and its expanded (2-sigma) uncertainty were
24 reported as 0.44 ± 0.07 and 0.40 ± 0.09 for heptane and toluene respectively.

25 Soot Yield: The values of the soot yield and its expanded uncertainty were reported as
26 $0.0149 \text{ kg/kg} \pm 0.0033 \text{ kg/kg}$ and $0.195 \text{ kg/kg} \pm 0.052 \text{ kg/kg}$ for heptane and toluene
27 respectively.

28 Natural Ventilation: The compartment had a 2 m (6.6 ft) by 2 m (6.6 ft) door in the middle of the
29 west wall. Some of the tests had a closed door and no mechanical ventilation (Tests 2, 7, 8, 13,
30 and 17), and in those tests the measured compartment leakage was an important consideration.
31 The test report lists leakage areas based on measurements performed before Tests 1, 2, 7, 8,
32 and 13. For the closed-door tests, the leakage area used in the simulations was based on the
33 last available measurement. The chronological order of the tests differed from the numerical
34 order. For Test 4, the leakage area measured before Test 2 was used. For Tests 10 and 16, the
35 leakage area measured before Test 7 was used.

36 Mechanical Ventilation: The mechanical ventilation system was used during Tests 4, 5, 10,
37 and 16, providing about 5 air changes per hour. The door was closed during Test 4 and open
38 during Tests 5, 10, and 16. The supply duct was positioned on the south wall, about 2 m (6.6 ft)
39 off the floor. An exhaust duct of equal area to the supply duct was positioned on the opposite
40 wall at a comparable location. The flow rates through the supply and exhaust ducts were
41 measured in detail during breaks in the testing, in the absence of a fire. During the tests, the
42 flows were monitored with a single bidirectional probe.

43 Please see "Report of Experimental Results for the International Fire Model Benchmarking and
44 Validation Exercise 3" (Hamins et al., 2006) for details concerning the NIST/NRC Experiments.



1
2 **Figure 3-7. Drawing of the NIST/NRC compartment.**

3

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1 **3.1.9 NIST Smoke-Alarm Experiments**

2 A series of experiments was conducted by NIST to measure the activation time of ionization and
3 photoelectric smoke alarms in a residential setting (Bukowski et al., 2008). Tests were
4 conducted in actual homes with representative sizes and floor plans, used actual furnishings
5 and household items for fire sources, and tested actual smoke alarms sold in retail stores at that
6 time. Thirty-six tests were conducted in two homes; twenty-seven in a single-story manufactured
7 home, and eight in a two-story home. Eight of the experiments that were conducted in the
8 single-story manufactured home were selected for model validation. Only tests that used a
9 flaming ignition source with a couch or mattress fuel package were considered; the cooking-oil
10 fires and tests that used a smoldering ignition source were not considered.

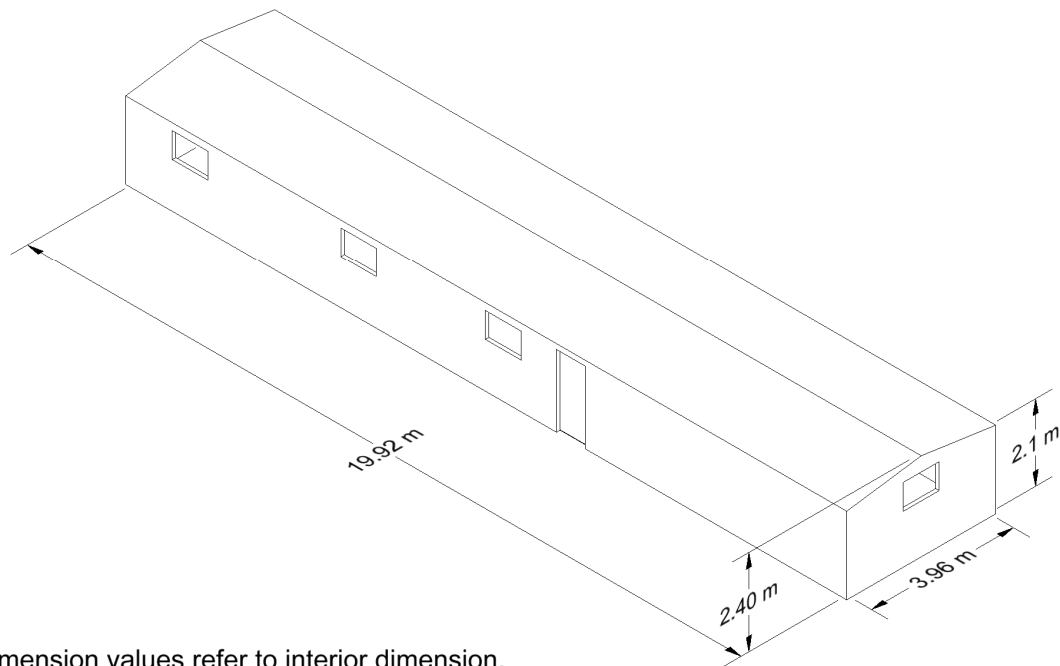
11 Geometry: A drawing of the manufactured home is shown in Figure 3-8. The ceiling was peaked
12 on the long axis, reaching a height of 2.4 m (7.9 ft). The outside walls were approximately 2.1 m
13 (6.9 ft) in height. The slope of the ceiling was approximately 8.4°. The doors to Bedroom #3 and
14 the bathroom were closed during all experiments.

15 Heat Release Rate: Although a load cell was used in the experiments to measure the mass-loss
16 rate of the fuel package, the mass-loss data were not reliable enough to reconstruct the HRR
17 curves for each test. Instead, the HRR curves were determined by approximating the fire growth
18 using a t -squared ramp. The parameters for the ramp were calibrated in FDS by using the
19 temperature measured at the highest thermocouple in the tree (2 cm (0.8 in) below the ceiling)
20 in the fire room (Bedroom #1). A time offset was used to align the predicted ceiling
21 thermocouple temperatures with the measured temperatures. This offset is reported as the time
22 at which the t -squared ramp begins. The t -squared calibration parameters and time offsets for
23 the HRR ramps are shown in Table 3-1. Additionally, the ignition source had a small effect on
24 the measured ceiling thermocouple temperatures. Therefore, the size of the ignition source was
25 approximated as either 3 kW or 7 kW and the time offset of the ignition source was also
26 calibrated by using the measured ceiling thermocouple temperatures.

27 Measurements: Groups of smoke alarms were located in the room of fire origin, at least one
28 bedroom, and in a central location. Five stations (Station A through Station E) containing
29 smoke-alarm arrays were mounted parallel to the ceiling.

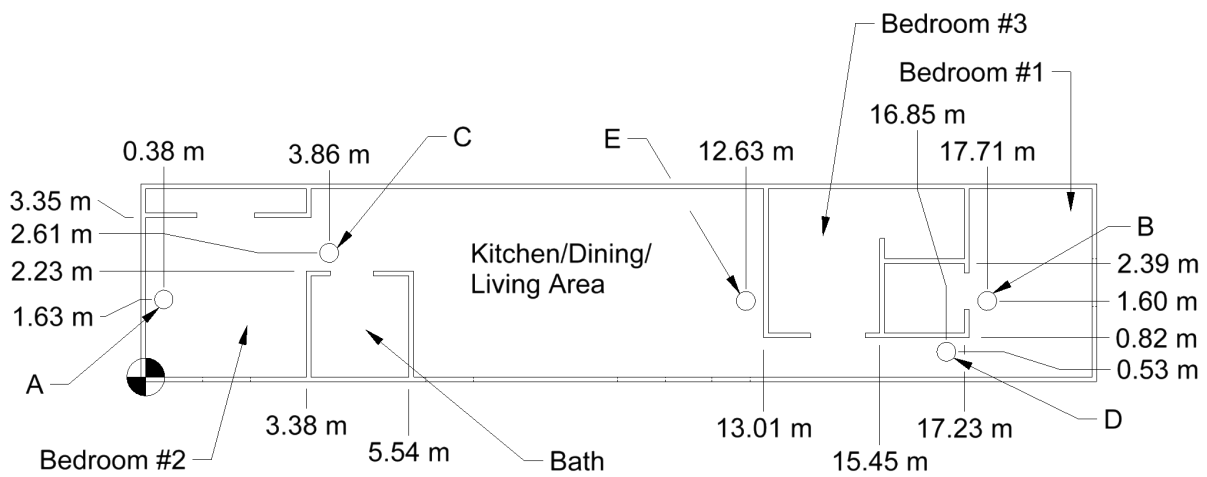
30 Please see the report "Performance of Home Smoke Alarms Analysis of the Response of
31 Several Available Technologies in Residential Fire Settings" (Bukowski et al., 2008) for details
32 concerning the NIST Smoke-Alarm Experiments.

33



Notes:

1. All dimension values refer to interior dimension.
2. The letters A-E refer to detector locations.
3. All walls are 10 cm thick.
4. All exterior doors and windows were closed during testing.
5. Doors to Bath and Bedroom #3 closed during testing.



1

2 **Figure 3-8. Drawing of the manufactured home used in the NIST Smoke-Alarm Tests.**

EXPERIMENTAL DATA

1 **Table 3-1. Parameters for the NIST Home Smoke-Alarm Experiments.**

Test No.	Fire Source	Fire Location	HRR (kW)	Ramp Time (s)	Time Offset (s)
SDC02	Chair	Living Room	150	180	20
SDC05	Mattress	Bedroom #1	200	180	20
SDC07	Mattress	Bedroom #1	350	180	50
SDC10	Chair	Living Room	150	180	40
SDC33	Chair	Living Room	100	180	10
SDC35	Chair	Living Room	100	180	10
SDC38	Mattress	Bedroom #1	120	180	25
SDC39	Mattress	Bedroom #1	200	180	25

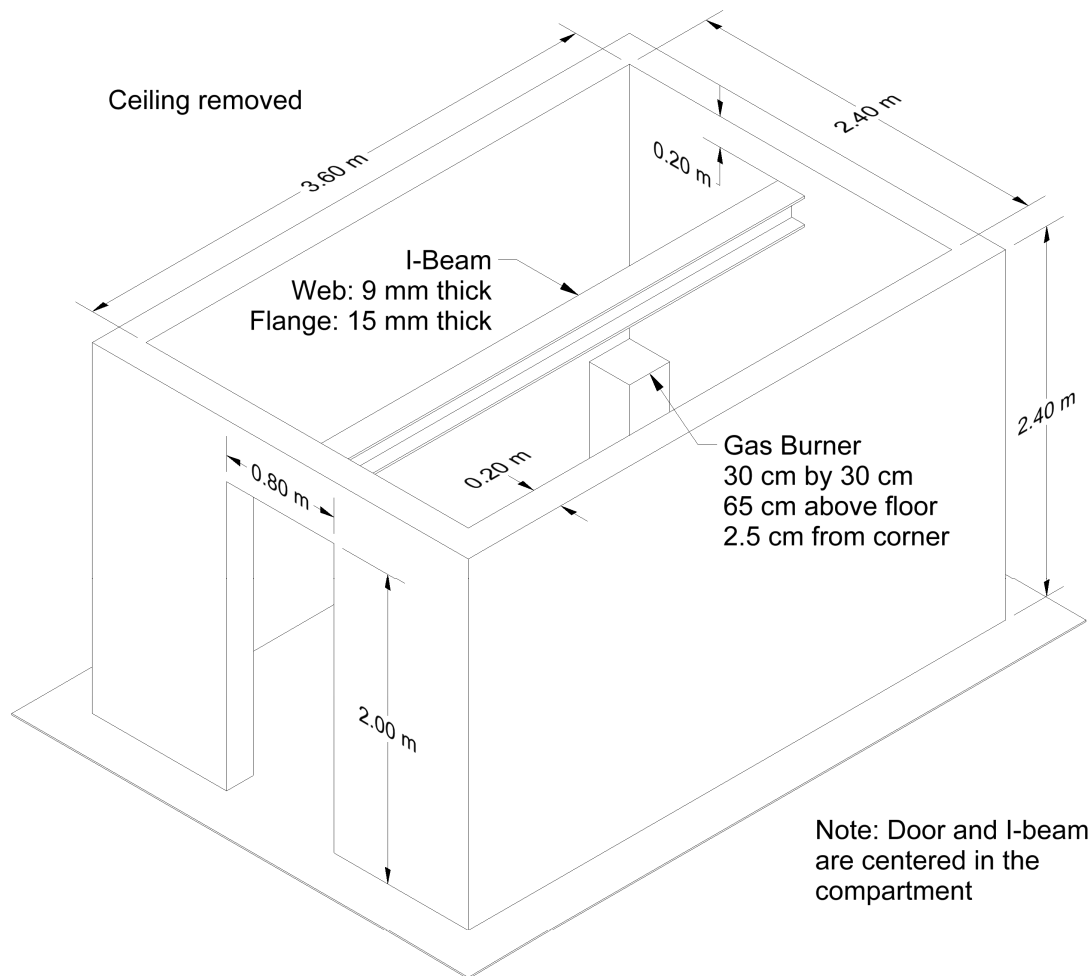
2 **3.1.10 SP Adiabatic Surface-Temperature Experiments**

3 In 2008, three compartment experiments were performed at SP Technical Research Institute of
4 Sweden under the sponsorship of Brandforsk, the Swedish Fire Research Board
5 (Wickström et al., 2009). The objective of the experiments was to demonstrate how plate
6 thermometer measurements in the vicinity of a simple steel beam can be used to supply the
7 boundary conditions for a multidimensional heat-conduction calculation for the beam.

8 Geometry: The experiments were performed inside a standard compartment designed for
9 corner fire testing. The compartment is 3.6 m (11.8 ft) deep, 2.4 m (7.9 ft) wide and 2.4 m
10 (7.9 ft) high and includes a door opening measuring 0.8 m (2.6 ft) by 2.0 m (6.6 ft) (Figure 3-9).
11 The room was constructed of 20-cm-thick (0.7-ft-thick) lightweight concrete blocks with a density
12 of $600 \text{ kg/m}^3 \pm 100 \text{ kg/m}^3$. A single steel beam was suspended 20 cm (0.7 ft) below the ceiling
13 along the centerline of the compartment.

14 Heat Release Rate: The fire was fueled by a propane burner with a constant HRR of 450 kW.
15 The top of the burner, with a square opening measuring 0.3 m (1 ft) by 0.3 m (1 ft), was placed
16 0.65 m (2.1 ft) above the floor, 2.5 cm (1 in) from the walls. The radiative fraction was assumed
17 to be 0.35.

18 Measurements: There were three measurement stations along the beam at lengths of 0.9 m
19 (2.9 ft) (Position A), 1.8 m (5.9 ft) (Position B), and 2.7 m (8.9 ft) (Position C) from the far wall
20 where the fire was either positioned in the corner (Tests 1 and 2) or the center (Test 3). The
21 beam in Test 1 was a rectangular steel tube filled with an insulation material. The beam in
22 Tests 2 and 3 was an I-beam.



1

2 **Figure 3-9. Drawing of SP AST Experiment.**

3 A second series of experiments involving plate thermometers was carried out in 2011
 4 (Sjöström et al., 2012). A vertical steel column 6 m (19.7 ft) long and 0.2 m (0.7 ft) in diameter
 5 was positioned in the center of 1.1 m (3.6 ft) and 1.9 m (6.2 ft) diesel-fuel and 1.1 m (3.6 ft)
 6 heptane pool fires. Gas, plate thermometer, and surface temperatures were measured at
 7 heights of 1 m (3.3 ft), 2 m (6.6 ft), 3 m (9.8 ft), 4 m (13.1 ft), and 5 m (16.4 ft) above the pool
 8 surface. These experiments are notable because the column is partially engulfed in flames.

9 Please see the reports "Verification Fire Tests on Using the Adiabatic Surface Temperature for
 10 Predicting Heat Transfer" (Wickström et al., 2009) and "Large Scale Test on Thermal Exposure
 11 to Steel Column Exposed to Pool Fires" (Sjöström et al., 2012) for details concerning the SP
 12 Adiabatic Surface-Temperature Experiments.

EXPERIMENTAL DATA

1 **3.1.11 Steckler Compartment Experiments**

2 Steckler, Quintiere, and Rinkinen (1979) performed a set of 55 compartment fire tests at NBS
3 in 1979.

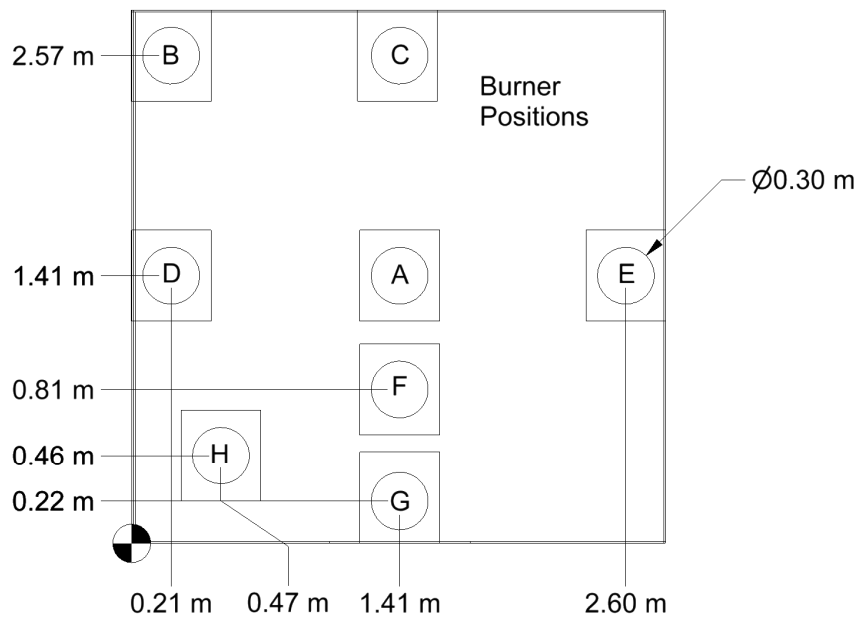
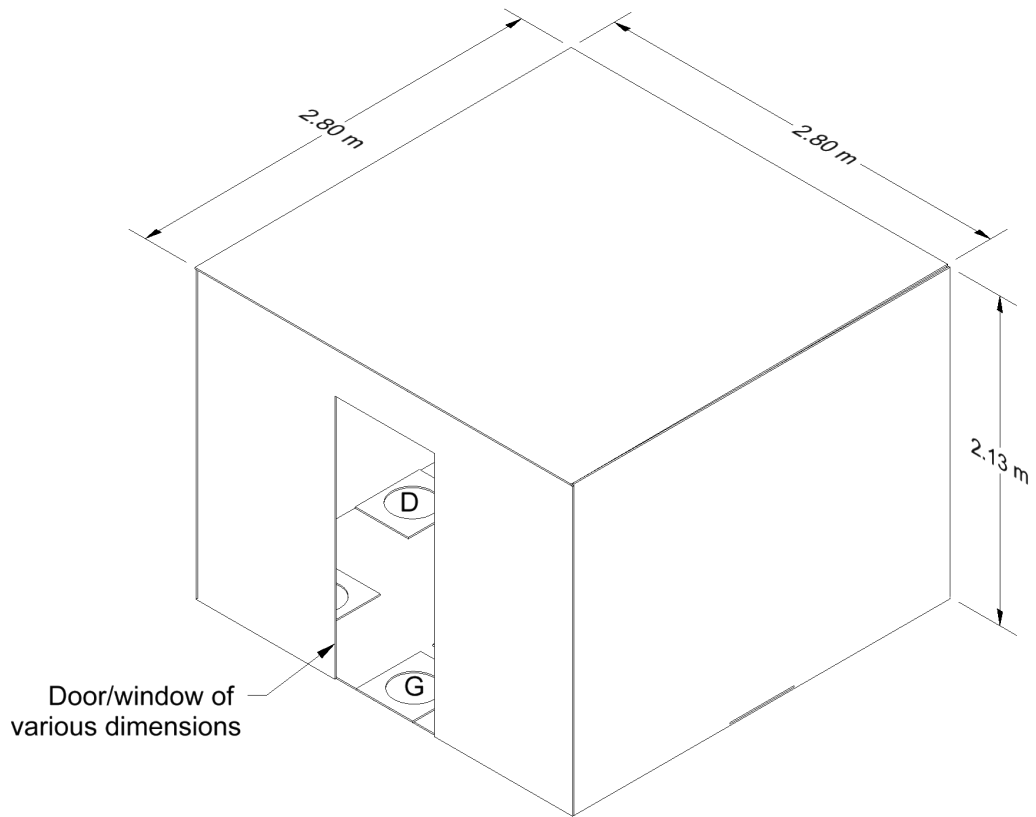
4 Geometry: The compartment was 2.8 m (9.2 ft) by 2.8 m (9.2 ft) by 2.13 m (7 ft) high, with a
5 single door of various widths, or alternatively a single window with various heights (Figure 3-10).

6 Wall Linings: The test report does not include a detailed description of the compartment.
7 However, an internal report by the test sponsor, Armstrong Cork Company, reports that the
8 compartment floor was composed of 19 mm (0.75 in) calcium silicate board on top of 12.7 mm
9 (0.5 in) plywood on wood joists. The walls and ceiling consisted of 12.7 mm (0.5 in) ceramic
10 fiber insulation board over 0.66-mm (0.03 in) aluminum sheet attached to wood studs.

11 Heat Release Rate: A methane burner 0.3 m (1 ft) in diameter was used to generate fires with
12 heat-release rates of 31.6 kW, 62.9 kW, 105.3 kW, and 158 kW. The radiative fraction was
13 assumed to be 0.20.

14 Measurements: Vertical profiles of velocity and temperature were measured in the doorway,
15 along with a single vertical profile of temperature within the compartment.

16 Please see the report "Flow Induced by Fire in a Compartment" (Steckler et al., 1979) for details
17 concerning the Steckler Compartment Experiments.



1
 2 **Figure 3-10. Drawing of Steckler Compartment.**

EXPERIMENTAL DATA

1 **3.1.12 UL/NIST Vent Experiments**

2 In 2012, the Fire Fighting Technology Group at NIST conducted experiments at Underwriters
3 Laboratories (UL[®]) in Northbrook, Illinois, to assess the change in compartment temperature
4 caused by the opening of one or two 1.2 m (3.9 ft) square ceiling vents (Opert, 2012).

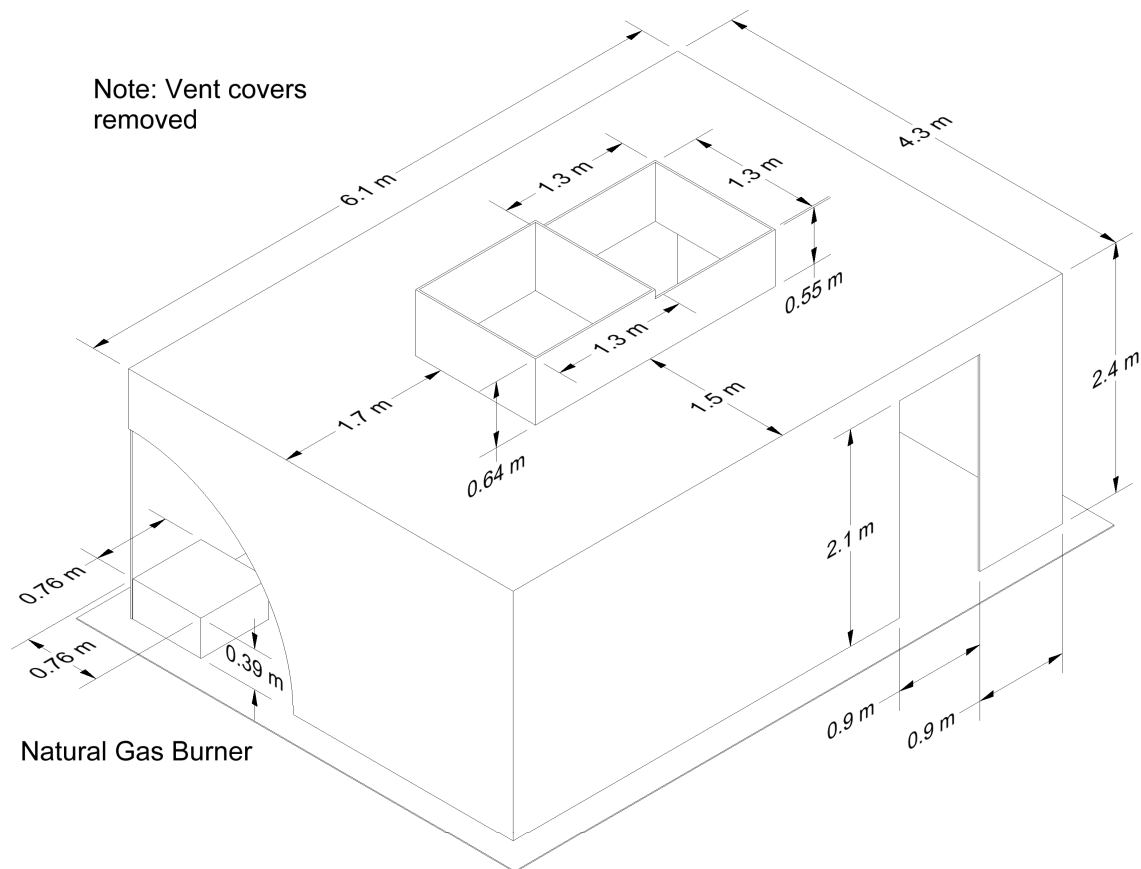
5 Geometry: The 6.1 m (20 ft) by 4.3 m (14.1 ft) by 2.4 m (7.9 ft) compartment with a single door
6 opening is shown in Figure 3-11. Two vents, nominally 1.3 m (4.3 ft) by 1.3 m (4.3 ft), were
7 positioned side by side at the center of the ceiling.

8 Heat Release Rate: The natural-gas fires ranged in size from 500 kW to 2 MW. The radiative
9 fraction was assumed to be 0.25, typical of large natural-gas fires.

10 Ventilation: The two vents were opened and closed in such a way that during the four
11 experiments there were 31 discrete time intervals in which model predictions could be
12 compared to quasi-steady conditions.

13 Measurements: The compartment contained two vertical arrays of thermocouples; the door and
14 vents were instrumented with thermocouples and bidirectional velocity probes. Only the
15 thermocouple measurements were used to assess the HGL and ceiling-jet temperatures and
16 HGL depth.

17 Please see the report "Assessment of Natural Vertical Ventilation for Smoke and Hot Gas Layer
18 Control in a Residential Scale Structure" (Opert, 2012) for details concerning the UL/NIST Vent
19 Experiments.



1
2 **Figure 3-11. Drawing of UL/NIST Experiment.**

3 **3.1.13 UL/NFPRF Sprinkler, Vent, and Draft Curtain Experiments**

4 In 1997, a series of 34 heptane spray burner experiments was conducted at the Large Scale
5 Fire Test Facility at Underwriters Laboratories (UL) in Northbrook, Illinois (Sheppard and
6 Stepan, 1997). The experiments were divided into two test series. Series I consisted of
7 twenty-two 4.4 MW fire experiments. Series II consisted of twelve 10 MW fire experiments. The
8 objective of the experiments was to characterize the temperature and flow field for fire scenarios
9 with a controlled heat-release rate in the presence of sprinklers, draft curtains, and smoke and
10 heat vents.

11 **Geometry:** The Large Scale Fire Test Facility at UL contains a 37 m (120 ft) by 37 m (120 ft)
12 main fire test cell, equipped with a 30.5 m (100 ft) by 30.5 m (100 ft) adjustable height ceiling.
13 The ceiling was raised to a height of 7.6 m (24.9 ft) and instrumented with thermocouples and
14 other measurement devices. Sheet metal, 1.2 mm (0.05 in) thick and 1.8 m (5.9 ft) deep, was
15 suspended from the ceiling for 16 of the 22 Series I tests, enclosing an area of about 450 m²
16 (4850 ft²) and 49 sprinklers. The curtains were in place for all of the Series II tests.

17 **Wall Linings:** The ceiling was constructed of 0.6 m (2 ft) by 1.2 m (3.9 ft) by 1.6 cm (0.6 in) UL
18 fire-rated Armstrong Ceramaguard® (Item 602B) ceiling tiles. The manufacturer reported the

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1 thermal properties of the material to be: specific heat 753 J/(kg·K), thermal conductivity
2 0.0611 W/(m·K), and density 313 kg/m³.

3 Heat Release Rate: The heptane spray burner consisted of a 1 m (3.3 ft) by 1 m (3.3 ft) square
4 of 1.3 cm (0.5 in) pipe supported by four cement blocks 0.6 m (2 ft) off the floor. Four atomizing
5 spray nozzles were used to provide a free spray of heptane that was then ignited. For all but
6 one of the Series I tests, the total heat-release rate from the fire was manually ramped up
7 following a *t*-squared curve to a steady-state in 75 s (150 s was used in Test I-16). The fire was
8 ramped to 10 MW in 75 s for the Series II tests. The fire growth curve was followed until a
9 specified fire size was reached or the first sprinkler activated. After either of these events, the
10 fire size was kept at that level until conditions reached roughly a steady state (i.e., the
11 temperatures recorded near the ceilings remained steady and no more sprinkler activations
12 occurred).

13 The heat release rate from the burner was confirmed by placing it under the large product
14 calorimeter at UL, ramping up the flow of heptane in the same manner as in the tests, and
15 measuring the total and convective heat-release rates. It was found that the convective
16 heat-release rate was 0.65 ± 0.02 of the total. This corresponds to a radiative fraction of 0.35.

17 Sprinklers: Central ELO-231 (Extra Large Orifice) uprights were used for all the tests. The orifice
18 diameter of this sprinkler is reported by the manufacturer to be nominally 1.6 cm (0.6 in); the
19 reference activation temperature is reported by the manufacturer to be 74°C (165°F). The RTI
20 (Response Time Index) and C-factor (Conductivity factor) were reported by UL to be
21 $148 \text{ (m}\cdot\text{s)}^{0.5}$ and $0.7 \text{ (m/s)}^{0.5}$ respectively. When installed, the sprinkler deflector was located
22 8 cm (3 in) below the ceiling. The thermal element of the sprinkler was located 11 cm (4 in)
23 below the ceiling. The sprinklers were installed with nominal 3 m by 3 m (exact 10 ft by 10 ft)
24 spacing in a system designed to deliver a constant $0.34 \text{ L/(s}\cdot\text{m}^2)$ discharge density when
25 supplied by a 131-kPa (19-psi) discharge pressure.

26 Ventilation: UL listed double-leaf fire vents with steel covers and a steel curb were installed in
27 the adjustable-height ceiling. Each vent was designed to open manually or automatically. The
28 vent doors were recessed into the ceiling by about 0.3 m (1 ft).

29 Please see the report “An Experimental Data Set for the Accuracy Assessment of Room Fire
30 Models” (McGrattan et al., 1998) for details concerning the UL/NFPRF Sprinkler, Vent, and Draft
31 Curtain Experiments.

32 **3.1.14 U.S. Navy High-Bay Hangar Experiments**

33 The U.S. Navy (USN) sponsored a series of 33 experiments within two hangars examining fire
34 detection and sprinkler activation in response to spill fires in large enclosures. Experiments were
35 conducted using JP-5 and JP-8 fuels in two Navy high-bay aircraft hangars located in the Naval
36 Air Stations in Barber’s Point, Hawaii, and Keflavik, Iceland (Gott et al., 1997). Eleven
37 experiments were conducted in Hawaii, twenty-two in Iceland.

38 Geometry: The Hawaii experiments were conducted in a 15 m high (49 ft high) hangar
39 measuring 97.8 m (321 ft) in length and 73.8 m (242 ft) in width. The Iceland experiments were
40 conducted under a 22 m (72 ft) barrel-vault ceiling in a hangar measuring 45.7 m (150 ft) by
41 73.8 m (242 ft).

42 Heat Release Rate: The fires in Hawaii were fueled by jet fuel in pans ranging from 0.09 m^2
43 (1 ft^2) to 4.9 m^2 (52.7 ft^2) in area with heat-release rates varying from 100 kW to 7.7 MW. The
44 burner was placed in the center of the room on a scale. The fires in Iceland were fueled by JP-5

1 and JP-8, ranging in size from 0.06 m² (0.6 ft²) to 20.9 m² (225 ft²) and the heat release rates
2 ranged from 100 kW to approximately 33 MW. The radiative fraction was assumed to be 0.35.

3 Measurements: Both facilities were equipped with a number of detection devices, including
4 thermocouples, electronic smoke and spot heat detectors, projected-beam smoke detectors,
5 combination UV/IR optical flame detectors, and line-type heat detectors, as well as sprinklers.
6 Measurements were recorded at a large number of locations, allowing a thorough profile of
7 compartment behavior.

8 Please see the report “Analysis of High Bay Hanger Facilities for Fire Detection Sensitivity and
9 Placement” (Gott et al., 1997) for details concerning the U.S. Navy High Bay Hangar
10 Experiments.

11 **3.1.15 Vettori Ceiling Sprinkler Experiments**

12 Vettori (1998) analyzed a series of 45 experiments conducted at NIST that were intended to
13 compare the effects of different ceiling configurations on the activation times of quick-response
14 residential pendent sprinklers. The test parameters consisted of two ceiling configurations, three
15 fire-growth rates, and three burner locations—a total of 18 unique test configurations with sets
16 of two or three replicates each.

17 Geometry: A diagram of the test structure is displayed in Figure 3-12. The ceiling was either
18 obstructed, with parallel beams 3.8 cm (1.5 in) wide by 0.24 m (0.8 ft) deep placed 0.41 m
19 (1.3 ft) on center, or smooth, in which the beams were covered by a sheet of gypsum board.

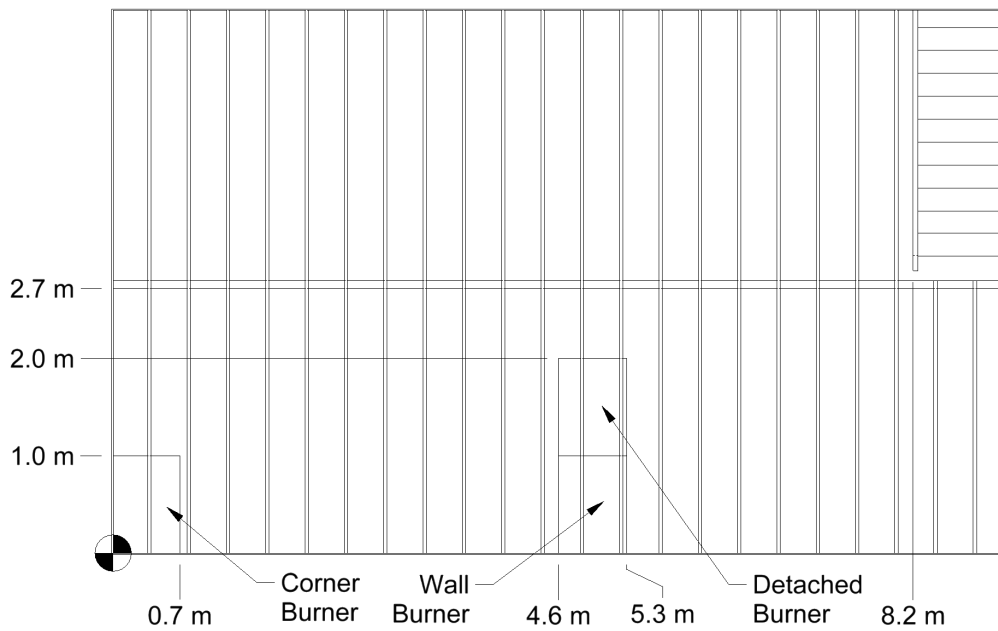
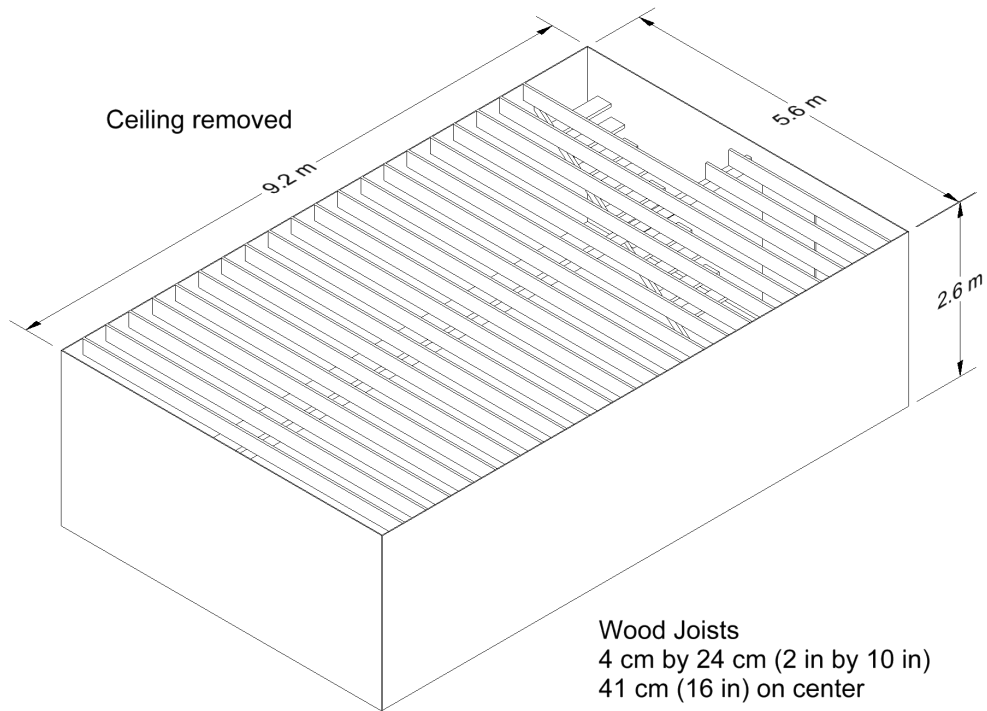
20 Heat Release Rate: The fire was fueled by a computer-controlled methane gas burner to mimic
21 a standard *t*-squared fire-growth rate with either a slow, medium, or fast ramp-up. Tests were
22 conducted with the burner placed in a corner of the room, against an adjacent wall, or in a
23 location removed from any wall.

24 Measurements: Measurements were taken to record sprinkler activation time, temperatures at
25 varying heights and locations within the room, and ceiling-jet velocities at several other
26 locations.

27 Vettori (2003) analyzed a similar set of sprinkler experiments involving ceilings of various
28 slopes. Because the empirical correlations and zone models lack the necessary physics to
29 model these experiments, only the FDS results are included in this study.

30 Please see the reports “Effect of a Beamed, Sloped, and Sloped Beamed Ceiling on the
31 Activation Time of a Residential Sprinkler” (Vettori, 1998) and “Effect of an Obstructed Ceiling
32 on the Activation Time of a Residential Sprinkler” (Vettori, 2003) for details concerning the
33 Vettori Flat Ceiling Sprinkler Experiments.

EXPERIMENTAL DATA



1
2 **Figure 3-12. Drawing of Vettori Flat Ceiling Sprinkler Experiments.**

3

1 **3.1.16 VTT Large Hall Experiments**

2 Hostikka et al. (2001) studied the movement of smoke in a large hall with a sloped ceiling.

3 Geometry: The tests were conducted inside the VTT Technical Research Centre of Finland Fire
4 Test Hall, with dimensions of 19 m (62 ft) high by 27 m (87 ft) long by 14 m (46 ft) wide
5 (Figure 3-13). The walls and ceiling of the test hall consisted of a 1-mm-thick (0.04-in-thick)
6 layer of sheet metal on top of a 5 cm (2 in) layer of mineral wool. The floor was constructed of
7 concrete. The report does not provide thermal properties of these materials.

8 Heat Release Rate: The fires were fueled by a single circular pan of heptane with its center
9 located 16 m (52.5 ft) from the west wall and 7.2 m (23.6 ft) from the south wall. The HRR
10 ranged from 2 MW to 4 MW. The pan had a diameter of 1.2 m (3.9 ft) for Case 1 and 1.6 m
11 (5.2 ft) for Cases 2 and 3. In each case, the fuel surface was 1 m (3.3 ft) above the floor. The
12 trays were placed on load cells and the HRR was calculated from the mass-loss rate. The
13 radiative fraction was assumed to be 0.35, typical of liquid hydrocarbon fires.

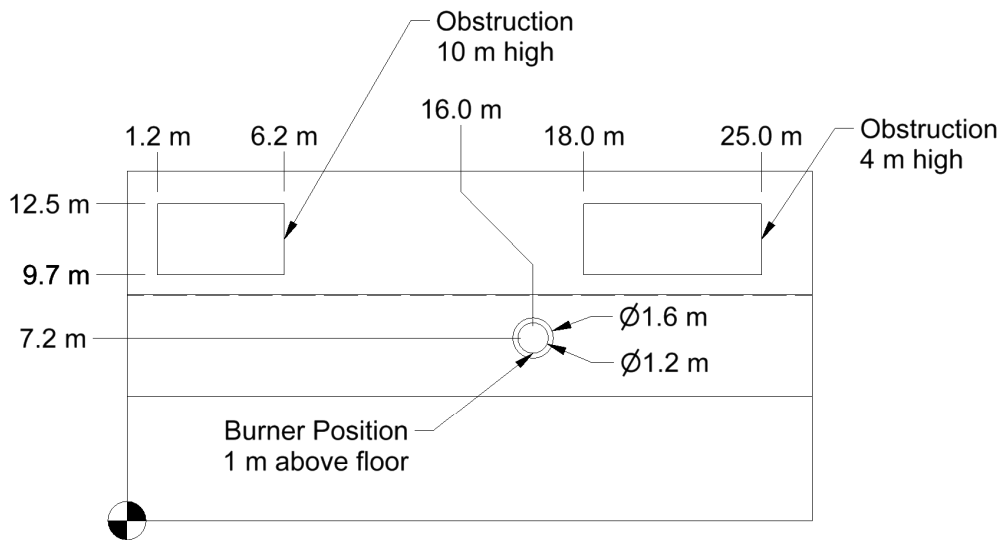
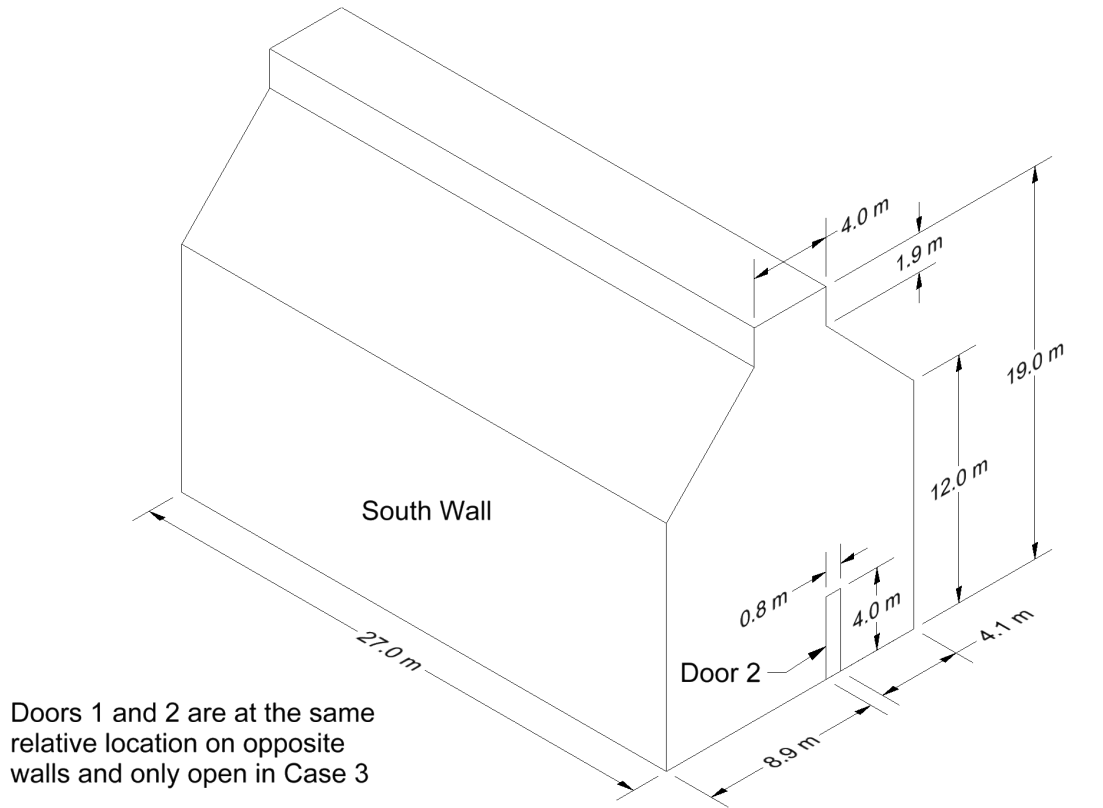
14 Natural Ventilation: In Cases 1 and 2, all doors were closed and ventilation was restricted to
15 infiltration through the building envelope. Precise information on air infiltration during these tests
16 is not available. Personnel who conducted the experiments recommend a leakage area of about
17 2 m² (21.5 ft²), distributed uniformly throughout the enclosure. By contrast, in Case 3, the doors
18 located in each end wall (Doors 1 and 2 respectively) were open to the external ambient
19 environment. These doors were each 0.8 m (2.6 ft) wide by 4 m (13.1 ft) high and were located
20 in such a way that their centers were 9.3 m (30.5 ft) from the south wall.

21 Mechanical Ventilation: The test hall had a single mechanical exhaust duct, located in the roof
22 space, running along the center of the building. This duct had a circular section with a diameter
23 of 1 m (3.3 ft), and opened horizontally to the hall at a distance of 12 m (39.4 ft) from the floor
24 and 10.5 m (34.4 ft) from the west wall. Mechanical exhaust ventilation was operational for
25 Case 3, with a constant-volume flow rate of 11 m³/s (388 ft³/s) drawn through the exhaust duct.

26 Measurements: Three vertical arrays of thermocouples, plus two thermocouples in the plume,
27 were used to measure the HGL temperature, HGL height, and plume temperature. The HGL
28 temperature and height were reduced from an average of the three thermocouple arrays.

29 Please see the report "Experimental Study of the Localized Room Fires" (Hostikka, et al., 2001)
30 for details concerning the VTT Large Hall Experiments.

EXPERIMENTAL DATA



1
2 **Figure 3-13. Drawing of VTT Test Hall.**

1 **3.1.17 WTC Spray Burner Experiments**

2 As part of its investigation of the World Trade Center (WTC) disaster, the Building and Fire
3 Research Laboratory at NIST conducted several series of fire experiments both to gain insight
4 into the observed fire behavior and to validate FDS for use in reconstructing the fires. The first
5 series of experiments involved a relatively simple compartment with a liquid spray burner and
6 various structural elements with varying amounts of sprayed fire-resistive materials
7 (Hamins et al., 2005).

8 Geometry: A diagram of the compartment is shown in Figure 3-14. The overall enclosure was
9 rectangular, as were the vents and most of the obstructions. The compartment walls and ceiling
10 were made of 2.5 cm (1 in) thick calcium silicate board. The manufacturer provided the thermal
11 properties of the material used in the calculation. The density was 737 kg/m^3 and the
12 conductivity was 0.12 W/m/K . The specific heat ranged from $1.17 \text{ kJ/kg/}^\circ\text{K}$ at 93°C (200°F) to
13 $1.42 \text{ kJ/kg/}^\circ\text{K}$ at 425°C (800°F). This value was assumed for higher temperatures. The steel
14 used to construct the column and truss flanges was 0.6 cm (0.25 in) thick. The density of the
15 steel was assumed to be $7,860 \text{ kg/m}^3$ and its specific heat was assumed to be $0.45 \text{ kJ/kg/}^\circ\text{K}$.

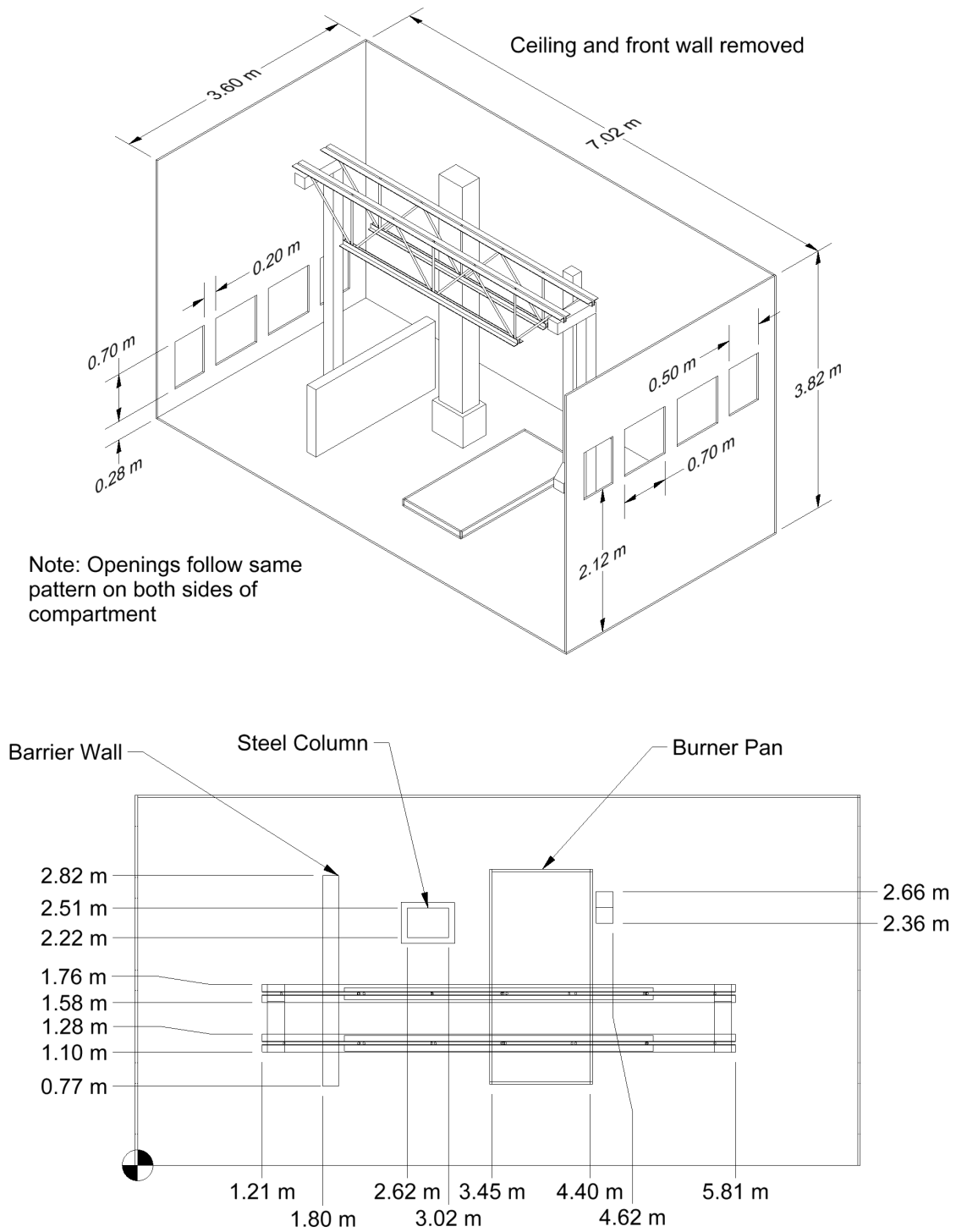
16 Heat Release Rate: Spray nozzles were used to inject liquid fuel downward into a 1 m (3.3 ft) by
17 2 m (6.6 ft) steel pan. Two fuels were used in the experiments. The properties of the fuels were
18 obtained from measurements made on a series of unconfined burns that are cited in the test
19 report. The first fuel was a blend of isomers of heptane, C_7H_{16} . Its soot yield was measured to
20 be 1.5 percent. The second fuel was a mixture (40 percent to 60 percent by volume) of toluene,
21 C_7H_8 , and heptane. The radiative fraction for the heptane blend was 0.44; for the
22 heptane/toluene mixture it was 0.39.

23 Ventilation: The compartment was naturally ventilated by way of openings at either end of the
24 compartment. The air moved from the lower towards the higher openings.

25 Measurements: The instrumentation consisted of vertical arrays of thermocouples, gas sampling
26 probes for oxygen, carbon dioxide, and carbon monoxide concentrations, smoke concentration,
27 unprotected and protected steel temperatures, exterior and interior wall temperatures, heat flux,
28 and velocity.

29 Please see the report "Federal Building and Fire Safety Investigation of the World Trade Center
30 Disaster; Experiments and Modeling of Structural Steel Elements Exposed to Fire"
31 (Hamins et al., 2005) for details concerning the WTC Spray Burner Experiments.

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1
2 **Figure 3-14. Drawing of the WTC Experiment.**

3

3.2 Summary of Experimental Parameters

Table 3-2 provides a summary of the major parameters for all the experiments used in the validation study. The basic parameters are defined as follows:

\dot{Q}	The heat release rate of the fire (kW)
D	The diameter of the fire (m); for non-circular burners, $D \cong \sqrt{4A/\pi}$
H	The height of the compartment (m)
L	The length of the compartment (m); i.e., the longer lateral dimension
W	The width of the compartment (m); i.e., the shorter lateral dimension
L_f	The length of the flame (m)
r_{cj}	The radial distance from the plume centerline to a ceiling target or detector (m)
r	The distance between the fire and a target (m)
φ	Equivalency ratio, which relates the energy release of the fire to the energy release that can be supported by the mass flow rate of oxygen into the compartment

To characterize the range of applicability of the validation study, Table 3-3 lists various normalized parameters that can be used to determine whether a modeled fire scenario fits within the range of the experimental parameters. These parameters express, for instance, the size of the fire relative to the size of the room or the relative distance from the fire to critical equipment. This information is important because typical fire models are not designed for fires that are very small or very large in relation to the volume of the compartment or the ceiling height. For a given set of experiments and NPP fire scenarios, the user can calculate the relevant normalized parameters. These parameters will either be inside, outside, or on the margin of the validation parameter space.

23

24

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1 **Table 3-2. Summary of major experiment parameters.**

Experiment	Experiment Parameters									
	\dot{Q} (kW)	D (m)	H (m)	\dot{Q}^*	L_f/H	ϕ	W/H	L/H	r_{cj}/H	r/D
ATF Corridors	50 to 500	0.5	2.4	0.3 to 3.3	0.3 to 0.9	0.0 to 0.1	0.8	7.1	0.8 to 6.0	N/A
Fleury	100 to 300	0.3 to 0.6	Open	0.3 to 5.5	Open	Open	Open	Open	Open	0.8 to 8
FM/SNL	470 to 2000	0.9	6.1	0.6 to 2.4	0.3 to 0.6	0.0 to 0.2	2.0	3.0	0.2 to 0.3	N/A
iBMB*	3500, 400	1.13, 0.79	5.7, 5.6	2.4, 0.7	0.8, 0.3	0.6, 0.1	0.6	0.6	N/A	N/A
LLNL	50 to 400	0.6	4.5	0.2 to 1.5	0.1 to 0.4	0.1 to 0.4	0.9	1.3	0.3 to 1.0	N/A
NBS Multi-Room	110	0.3	2.4	1.5	0.5	0.0	1.0	5.1	N/A	N/A
NIST/NRC	350 to 2200	1.0	3.8	0.3 to 2.0	0.3 to 1.0	0.0 to 0.3	1.9	5.7	0.3 to 2.1	2 to 4
SP AST	450	0.3	2.4	6.1	0.9	0.1	1.0	1.5	N/A	N/A
Steckler	32 to 158	0.3	2.1	0.8 to 3.8	0.3 to 0.7	0.0 to 0.5	1.3	1.3	N/A	N/A
UL/NFPRF	4400 to 10,000	1.0	7.6	4.0 to 9.1	0.7 to 1.0	N/A	4.9	4.9	0.6 to 3.9	N/A
UL/NIST Vents	500 to 2000	0.9	2.4	0.7 to 2.6	0.8 to 1.6	0.2 to 0.6	1.8	2.5	1.0 to 2.3	N/A
USN Hawaii	100 to 7700	0.3 to 2.5	15	0.7 to 1.3	0.1 to 0.4	N/A	4.9	6.5	0 to 1.2	N/A
USN Iceland	100 to 15,700	0.3 to 3.4	22	0.7 to 1.3	0.0 to 0.3	N/A	2.1	3.4	0 to 1.0	N/A
Vettori Flat	1055	0.7	2.6	2.5	1.1	0.3	2.1	3.5	0.8 to 2.9	N/A
Vettori Sloped	1055	0.7	2.5	2.5	1.2	0.3	2.2	2.9	N/A	N/A
VTT Hall	1860 to 3640	1.2 to 1.6	19	1.0 to 1.1	0.2	0 to 0.09	1.0	1.4	0 to 0.6	N/A
WTC	1970 to 3240	1.6	3.8	0.6 to 0.9	0.8 to 1.1	0.3 to 0.5	0.9	1.8	0 to 0.8	0.3 to 1.3

* Where two values are present, the first is for the test from Benchmark Exercise #4 and the second is for the test from Benchmark Exercise #5.

2

1 **Table 3-3. Summary of normalized experimental parameters**

Quantity	Normalized Parameter	Definition	Experiment Range
Fire Froude Number	$\dot{Q}^* = \frac{\dot{Q}}{\rho_{\infty} c_p T_{\infty} D^2 \sqrt{gD}}$	Ratio of inertial and buoyancy-induced velocities. A typical accidental fire has a Froude number of order 1. Momentum-driven fire plumes, like jet flames, have relatively high values. Buoyancy-driven fire plumes have relatively low values.	0.2 to 9.1
Flame Length Ratio	$\frac{H_f + L_f}{H}$ $\frac{L_f}{D} = 3.7 \dot{Q}^{*2/5} - 1.02$	A convenient parameter for expressing the “size” of the fire relative to the height of the compartment. A value of 1 means that the flames reach the ceiling.	0.0 to 1.6
Ceiling-Jet Distance Ratio	$\frac{r_{cj}}{H}$	Ceiling-jet temperature and velocity correlations use this ratio to express the horizontal distance from target to plume.	0.0 to 6.0
Equivalence Ratio	$\varphi = \frac{\dot{Q}}{\Delta H_{O_2} \dot{m}_{O_2}}$ $\dot{m}_{O_2} = \begin{cases} 0.23 \times \frac{1}{2} A_0 \sqrt{H_0} & \text{(Natural)} \\ 0.23 \rho_{\infty} \dot{V} & \text{(Mechanical)} \end{cases}$	The equivalence ratio relates the energy release rate of the fire to the energy release that can be supported by the mass flow rate of oxygen into the compartment, \dot{m}_{O_2} . The fire is considered over- or underventilated based on whether φ is less than or greater than 1 respectively.	0.0 to 0.6
Compartment Aspect Ratio	$L/H \text{ or } W/H$	This parameter indicates the general shape of the compartment.	0.8 to 7.1
Radial Distance Ratio	$\frac{r}{D}$	This ratio is the relative distance from a target to the fire. It is important when calculating the radiative heat flux.	0.3 to 8

2

1 **3.3 Experimental Uncertainty**

2 The difference between a model's prediction and an experiment's measurement is a
3 combination of three components: (1) uncertainty in the measurement of the predicted quantity,
4 (2) uncertainty in the model input parameters, and (3) uncertainty in the model physics and
5 numerics. The first two components are related to uncertainty in the measured input and output
6 quantities. For example, consider the HGL temperature. First, the thermocouple measurements
7 used to calculate the HGL temperature have uncertainty. Second, the measurement of the
8 heat-release rate of the fire has uncertainty, and this uncertainty affects the predicted HGL
9 temperature. Third, the model itself, including its physical assumptions and numerical
10 approximations, has uncertainty. The objective of the validation study is to quantify this third
11 component, the *model uncertainty*. To do this, the first two components of uncertainty related to
12 the experimental measurements must be quantified. The combination of these two, the
13 *experimental uncertainty*, is the objective of this section.

14 For many of the test series considered in this report, the uncertainty of the measurements was
15 not documented in the experiment reports. Instead, estimates of measurement uncertainty are
16 made based on those few experiments that do include uncertainty estimates, and this
17 information is supplemented by engineering judgment.

18 In the following two subsections, each component of the experimental uncertainty is considered
19 separately. First, the uncertainty in the measurement of the predicted quantity of interest, such
20 as the surface temperature of the compartment, is considered. Second, the uncertainties of the
21 most important input parameters are propagated through simple models to quantify their effect
22 on the predicted quantity. Then, the uncertainties are combined through simple quadrature to
23 estimate the total experimental uncertainty.

24 Note that in this report, all uncertainties are expressed in relative form, as a percentage. The
25 uncertainty of a measurement is a combination of the *epistemic uncertainty* associated with the
26 various underlying measurements and assumptions and the *aleatory uncertainty* associated
27 with random variations in the experiment. Following the recommended guidelines for evaluating
28 and expressing the uncertainty of measurements (Taylor and Kuyatt, 1994), the epistemic and
29 aleatory uncertainty values are combined through quadrature resulting in a *combined relative*
30 *standard uncertainty*.

31 **3.3.1 Measurement Uncertainty**

32 Because most of the experiments described in Section 3.1 were reported with little or no
33 information about the uncertainty of the measurements, much of this section is based on the
34 uncertainty analysis contained in the test report of the NIST/NRC Compartment Fire
35 Experiments, NUREG/CR-6905 (2003). The types of measurements described in this report are
36 the ones most commonly used in large-scale fire experiments. They include thermocouples for
37 gas- and surface-temperature measurements, heat-flux gauges, smoke and gas analyzers, and
38 pressure sensors.

39 Note that the experimental uncertainties reported in NUREG/CR-6905 are reported in the form
40 of 95 percent confidence intervals, or two standard deviations of the reported value. In this
41 report, however, the uncertainty of all measurements and model predictions are reported as a
42 single standard deviation.

1 **3.3.1.1 Thermocouples**

2 Thermocouples are used to measure both gas and surface temperatures. They come in a
3 variety of sizes and are constructed of different types of metals. Some are shielded or aspirated
4 to limit the influence of thermal radiation from remote sources. In NUREG/CR-6905 (2003),
5 Hamins et al. estimate the uncertainty of the various thermocouple measurements. Estimates of
6 the combined relative standard uncertainty fall in a range between 2.5 percent and 7.5 percent.
7 Because it is not possible to analyze the thousands of thermocouple measurements made in the
8 experiments reported in Section 3.1, the relative standard uncertainty applied to all
9 thermocouple measurements is 5 percent.

10 **3.3.1.2 Heat Flux Gauges**

11 For the NIST/NRC Compartment Fire Experiments (NUREG/CR-6905, 2003), four types of
12 heat-flux gauges were used, some of which measured the total heat flux and others of which
13 measured only the radiation heat flux. The uncertainty associated with a heat-flux measurement
14 depends on many factors, including gauge characteristics and the calibration conditions and
15 accuracy, as well as the incident flux modes (convective, radiative, and/or conductive)
16 (Bryant et al., 2003). Typically, the reported relative standard uncertainty of heat-flux gauges
17 varies from about 2.5 percent to 5 percent, with the measurement uncertainty dominated by
18 uncertainty in the calibration and repeatability of the measurement. For all of the experiments
19 described in Section 3.1, a combined relative standard uncertainty of 5 percent is suggested.

20 **3.3.1.3 Gas Analyzers**

21 Gas concentrations were measured in two sets of experiments conducted at NIST, the
22 NIST/NRC experiments (NUREG/CR-6905, 2003) and the WTC experiments
23 (Hamins et al., 2005). The volume fractions of the combustion products, carbon monoxide (CO)
24 and carbon dioxide (CO₂), were measured using gas sampling in conjunction with
25 non-dispersive infrared analyzers, while the oxygen (O₂) volume fraction was typically measured
26 using a paramagnetic analyzer. Gases were extracted through stainless steel or other types of
27 lines and were pumped from the compartment and passed through the analyzers. For several
28 reasons, water in the sample was typically filtered, so the reported results are denoted as "dry".
29 Analyzers were calibrated through the use of standard gas mixtures, with low relative
30 uncertainties. Problems with the technique might involve instrument drift, analyzer response,
31 incomplete and partial drying of sample gases, or (in the case in which drying is not used)
32 undetermined amounts of water vapor in the oxygen cell, which result in inaccurate readings.

33 For the NIST/NRC experiments, the species were measured in both the upper and lower layers.
34 The relative standard uncertainty in the measured values was about 2 percent for both the O₂
35 depletion and the CO₂ measurements. The largest contributors were the uncertainty in the
36 composition of the calibration gas and the possibility of an undetermined amount of water vapor
37 in the sample.

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1 **3.3.1.4 Smoke Light Extinction Calculation**

2 The smoke concentration was measured in the NIST/NRC experiments
3 (NUREG/CR-6905, 2003) using laser transmission at 632.8 nm. The reported mass
4 concentration of smoke, m_s''' , was computed using the following expression:

$$m_s''' = \frac{\ln(I_0/I)}{\varphi_s L} \quad (3-1)$$

5 where L is the path length, I and I_0 are the laser signal and reference signal respectively, and
6 φ_s is the specific extinction coefficient, which has a nearly universal value of $8.7 \text{ m}^2/\text{g} \pm 5$
7 percent for hydrocarbons (Mulholland and Croakin, 2000). The epistemic uncertainty of this
8 measurement was reported to be 9 percent in NUREG/CR-6905, with the dominant contribution
9 to the uncertainty coming from drift in the laser measurement. Repeatability of the smoke
10 measurement was investigated for the NIST/NRC experiments. The mean difference between
11 replicate measurements was about 11 percent. Therefore, combining the epistemic and aleatory
12 uncertainties through quadrature leads to a relative standard uncertainty of 14 percent.

13 **3.3.1.5 Pressure Gauges**

14 The uncertainty in pressure measurements is typically small, but depends on the sensor type
15 and calibration. In NIST/NRC experiments, the differential pressure gauge used was
16 temperature-compensated, highly linear, and very stable. An estimate of the epistemic
17 uncertainty was given as 0.5 percent.

18 **3.3.1.6 Oxygen-Consumption Calorimeters**

19 For all of the experiments described in Section 3.1, the HRR is determined either by
20 oxygen-consumption calorimetry or by the mass-loss rate multiplied by the fuel heat of
21 combustion. The accuracy of each method varies roughly between 2.5 percent, where the fire is
22 small and the fuel stoichiometry is well understood, and 13 percent, where the fire is large or the
23 smoke is not completely captured or the fuel stoichiometry is not well understood. In
24 NUREG/CR-6905, the relative standard uncertainty of a 2-MW heptane spray fire is estimated
25 to be 7.5 percent. It is assumed that the uncertainty of the HRR for the other experiments is
26 comparable.

27 **3.3.1.7 Sprinkler and Detector Activation Times**

28 There are a variety of ways to measure the time at which a sprinkler actuates, a cable shorts, or
29 a detector alarms. For example, a thermocouple registers a rapid decrease in temperature when
30 a sprinkler opens. Changes in the electrical response of a detector or cable are essentially
31 instantaneous. For these reasons, the uncertainty in the reported activation or failure time of
32 various devices is, for all practical purposes, zero.

33 **3.3.2 Propagation of Input Parameter Uncertainty**

34 The empirical correlations described in Section 4.1 provide a convenient way to assess the
35 propagation of the uncertainty of the model input parameters. The more complex fire models
36 might require dozens of physical and numerical input parameters for a given fire scenario.
37 However, only a few of these parameters, when varied over their plausible range of values,
38 significantly impact the results. For example, the thermal conductivity of the compartment walls

1 does not significantly affect a predicted cable surface temperature, but the HRR of the fire does.
 2 The relatively simple empirical models identify the key parameters that impact the predicted
 3 quantity and they provide the means to quantify the functional relationship between model
 4 inputs and outputs.

5 **3.3.2.1 Gas and Surface Temperatures**

6 According to the McCaffrey, Quintiere, and Harkleroad (MQH) correlation, the HGL temperature
 7 rise, $T - T_0$, in a compartment fire is proportional to the HRR, \dot{Q} , raised to the two-thirds power:

$$T - T_0 = C\dot{Q}^{2/3} \quad (3-2)$$

8 Here, C is related to the geometry and thermal properties of the compartment and T_0 is a
 9 reference temperature, typically ambient temperature. Taking the first derivative of T with
 10 respect to \dot{Q} and writing the result in terms of differentials yields:

$$\frac{\Delta T}{T - T_0} \cong \frac{2}{3} \frac{\Delta \dot{Q}}{\dot{Q}} \quad (3-3)$$

11 This is a simple formula with which one can readily estimate the relative change in the model
 12 output quantity, $\Delta T/(T - T_0)$, caused by the relative change in the model input parameter $\Delta \dot{Q}/\dot{Q}$.
 13 In subsection 3.3.1.6, the uncertainty in the HRR of the validation experiments, $\Delta \dot{Q}/\dot{Q}$, was
 14 estimated to be 7.5 percent. Equation (3-3) indicates that a 7.5 percent increase in the HRR
 15 should lead to a 5 percent increase in the HGL temperature.

16 **3.3.2.2 HGL Depth**

17 Most of the experiments for which the HGL depth was predicted had at least one open door or
 18 window that effectively determined the steady-state HGL depth. Unlike all of the other predicted
 19 quantities, the HGL depth is relatively insensitive to the fire's HRR. It is largely determined by
 20 the height of the opening, and for this reason there is essentially no uncertainty associated with
 21 the model inputs that affect the layer depth.

22 **3.3.2.3 Gas and Smoke Concentration**

23 Most fire models assume that combustion product gases and soot, once beyond the flaming
 24 region of the fire, are passively transported throughout the compartment. The major products of
 25 combustion, such as CO_2 and water vapor, plus the major reactant, O_2 , are generated or
 26 consumed in direct proportion to the burning rate of the fuel, which is directly proportional to the
 27 HRR. The mass fraction of any species in the HGL is directly proportional to the product of its
 28 yield and the HRR.

29 For the experiments described in Section 3.1, the yields of the major product gases such as O_2
 30 and CO_2 from pure fuels such as methane gas and heptane liquid are known from the basic
 31 stoichiometry to a high level of accuracy. Thus, the relative uncertainty in the concentration of
 32 major product gases is the same as that of the HRR, 7.5 percent. The uncertainty in the smoke
 33 concentration, however, is a combination of the uncertainty of the HRR and the soot yield. The
 34 relative standard uncertainty of the soot yield of heptane reported in NUREG/CR-6905
 35 is 11 percent. The uncertainties for HRR and soot yield are combined through quadrature and
 36 the resulting expanded relative uncertainty is $(0.075^2 + 0.11^2)^{1/2} = 0.133$, or 13 percent.

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1 3.3.2.4 Pressure

2 In a closed and ventilated compartment, the average pressure, p (Pa), is governed by the
3 following equation:

$$\frac{dp}{dt} = \frac{\gamma - 1}{V} (\dot{Q} - \dot{Q}_{\text{loss}}) + \frac{\gamma p}{V} (\dot{V} - \dot{V}_{\text{leak}}) \quad (3-4)$$

4 where γ is the ratio of specific heats (about 1.4), V is the compartment volume (m^3), \dot{Q} is the
5 HRR (kW), \dot{Q}_{loss} is the sum of all heat losses to the walls (kW), \dot{V} is the net ventilation rate into
6 the compartment (m^3/s), and \dot{V}_{leak} is the leakage rate out of the compartment (m^3/s). The
7 leakage rate is a function of the compartment overpressure:

$$\dot{V}_{\text{leak}} = A_{\text{leak}} \sqrt{\frac{2(p - p_{\infty})}{\rho_{\infty}}} \quad (3-5)$$

8 where A_{leak} is the leakage area (m^2), p_{∞} is the ambient pressure (Pa), and ρ_{∞} is the ambient air
9 density (kg/m^3). The maximum compartment pressure is achieved when the pressure-rise term
10 in Eq. (3-4) is set to zero. Rearranging terms yields an estimate for the maximum pressure:

$$(p - p_{\infty})_{\text{max}} \cong \frac{\rho_{\infty}}{2} \left(\frac{(\gamma - 1)(\dot{Q} - \dot{Q}_{\text{loss}}) + \gamma p_{\infty} \dot{V}}{\gamma p_{\infty} A_{\text{leak}}} \right)^2 \quad (3-6)$$

11 The test report for the NIST/NRC experiments (NUREG/CR-6905) contains estimates of the
12 uncertainty in the HRR, ventilation rate, and leakage area. To calculate the uncertainty in the
13 maximum pressure rise resulting from the uncertainty in these three parameters, the
14 pressure-rise estimate in Eq. (3-6) was calculated using 1000 randomly selected sets of values
15 of the HRR, ventilation rate, and leakage area. These parameters were assumed to be
16 randomly distributed with mean values of 1000 kW, $1 \text{ m}^3/\text{s}$, and 0.06 m^2 and relative standard
17 uncertainties of 75 kW, $0.1 \text{ m}^3/\text{s}$, and 0.0021 m^2 . The mean values of these parameters were
18 typical of the NIST/NRC experiments, and the uncertainties were reported in the test report. The
19 resulting relative standard uncertainty in the pressure is 21 percent.

20 3.3.2.5 Heat Flux

21 The heat flux to a target or wall is a combination of direct thermal radiation from the fire and
22 convective and thermal radiation from the HGL. If the heat flux is predominantly caused by the
23 thermal radiation of the fire, it can be approximated using the point-source radiation model:

$$\dot{q}'' = \frac{\chi_r \dot{Q}}{4\pi r^2} \quad (3-7)$$

24 Where \dot{q}'' is the heat flux (kW/m^2), χ_r is the radiative fraction, \dot{Q} is the HRR (kW), and r is the
25 distance from the fire (m). The relative standard uncertainty of the heat flux is a combination of
26 the uncertainty in the radiative fraction and the HRR:

$$\frac{\delta \dot{q}''}{\dot{q}''} \cong \frac{\delta \dot{Q}}{\dot{Q}} + \frac{\delta \chi_r}{\chi_r} \quad (3-8)$$

1 NUREG/CR-6905 estimates the relative standard uncertainty of the radiative fraction of a
 2 heptane pool fire to be 8 percent. Combined with the 7.5 percent uncertainty in the HRR
 3 (through quadrature) yields an 11 percent relative standard uncertainty in the heat flux directly
 4 from a fire.

5 The heat flux, \dot{q}'' (kW/m²), to a cold surface resulting from the exposure to hot gases and not
 6 necessarily the fire itself is the sum of radiative and convective components:

$$\dot{q}'' = \varepsilon\sigma(T_{\text{gas}}^4 - T_{\infty}^4) + h(T_{\text{gas}} - T_{\infty}) \quad (3-9)$$

7 where ε is the surface emissivity, σ is the Stefan-Boltzmann constant, T_{gas} is the gas
 8 temperature, T_{∞} is the ambient temperature, and h is the convective heat-transfer coefficient.
 9 From the discussion above, the relative standard uncertainty in the gas temperature rise above
 10 ambient is 5 percent (resulting from an estimated uncertainty in the HRR of 7.5 percent). There
 11 is also uncertainty in the convective heat-transfer coefficient, but this is attributed to the model,
 12 not the experimental measurements. Thus, the uncertainty in the heat flux is largely a function
 13 of the uncertainty in the gas temperature, which is largely a function of the HRR. As was done
 14 for the pressure, 1000 randomly selected values of gas temperature with a mean of 300°C
 15 above ambient and a relative uncertainty of 5 percent resulted in a corresponding uncertainty
 16 of 9 percent in the heat flux.

17 In actual compartment fires, the heat flux to surfaces is a combination of direct thermal radiation
 18 from the fire and indirect radiation and convection from the hot gases. Given that the calculation
 19 of the former incurs a 11 percent relative standard uncertainty and the latter 9 percent, to
 20 simplify the analyses, a value of 10 percent is used for all heat-flux predictions.

21 3.3.2.6 Sprinkler Activation Time

22 The uncertainty in the reported sprinkler activation times is mainly because of uncertainties in
 23 the measured HRR, RTI (Response-Time Index), and activation temperature. There is a
 24 negligible uncertainty in the measured activation time itself, which is typically determined with a
 25 pressure transducer. To determine the effect of the uncertainties in the HRR, RTI, and activation
 26 temperature, consider the ordinary differential equation governing the temperature, T_d , of a
 27 sprinkler (Custer et al., 2008):

$$\frac{dT_d}{dt} = \frac{\sqrt{u}}{\text{RTI}}(T_{\text{gas}} - T_d) \quad (3-10)$$

28 Here, u and T_{gas} are the respective velocity and the temperature of the ceiling jet. According to
 29 Alpert's ceiling-jet correlation, the ceiling-jet temperature and velocity are proportional to the
 30 HRR raised to the power of 2/3 and 1/3 respectively. Given the relative standard uncertainty in
 31 the HRR of 7.5 percent, the uncertainties in the ceiling-jet temperature and velocity are thus 5
 32 percent and 2.5 percent respectively. As for the RTI and activation temperature, these values
 33 are measured experimentally and the uncertainties differ depending on the test procedure.
 34 Vettori (1998) reports that the RTI of the sprinklers used in his experiments is 56 (m·s)^{0.5} with a
 35 relative standard uncertainty of 11 percent and that the activation temperature is 68°C ± 2.4°C.
 36 This latter uncertainty estimate is assumed to represent one standard deviation. Assuming an
 37 ambient temperature of approximately 20°C, the relative standard uncertainty in the activation
 38 temperature is assumed to be 5 percent.

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1 Equation (3-10) was integrated 1000 times using random selections of the ceiling-jet
2 temperature and velocity, RTI, and activation temperature. The mean ceiling-jet temperature
3 was increased linearly at rates varying from 0.5°C/s to 2°C/s, which are consistent with the
4 variety of growth rates measured by Vettori. The mean ceiling-jet velocity was assumed to be
5 1 m/s. This procedure yielded a relative standard uncertainty in the sprinkler activation time
6 of 6 percent.

7 The activation times recorded by Vettori include two or three replicates for each configuration.
8 The standard deviation of the 45 measured activation times, normalized by the mean of each
9 set of replicates, was 6 percent, which is consistent with the result obtained above.

10 **3.3.2.7 Cable Failure Time**

11 The uncertainty in the reported cable failure times is mainly because of uncertainties in the
12 measured exposing temperature, cable diameter, and jacket thickness. The uncertainty in the
13 measured mass per unit length of the cable is assumed to be negligible. To determine the
14 uncertainty in the cable failure time, the heat-conduction equation in the THIEF model was
15 solved numerically using 10,000 random selections of the exposing temperature, cable
16 diameter, and jacket thickness. The cable diameter was varied from 16.25 mm to 16.35 mm and
17 the jacket thickness was varied from 1.45 mm to 1.55 mm. The uncertainty in the exposing
18 temperature of the cylindrical heater was assumed to be 2.5 percent, the lower bound of the
19 range of uncertainty estimates for thermocouple measurements given in subsection 3.3.1.1. The
20 mass per unit length of the cable was assumed to be 0.529 kg/m and the ambient temperature
21 was assumed to be 20°C. This procedure yielded an estimated relative standard uncertainty in
22 the cable failure time of 12 percent.

23 **3.3.2.8 Smoke Detector Activation Time**

24 There is a single set of experiments with which to evaluate model predictions of smoke-detector
25 activation time, the NIST Home Smoke Alarm Experiments. The test report
26 (Bukowski et al., 2008) does not include detailed information about the alarm mechanism within
27 the various smoke detectors used in the experiments. Thus, from a modeling standpoint, these
28 devices are “black boxes” and their activation can only be discerned from a variety of empirical
29 techniques, the most popular of which is to assume that the smoke detector behaves like a
30 sprinkler or heat detector whose activation is governed by Eq. (3-10) with a low activation
31 temperature and RTI. Bukowski and Averill (1998) suggest that an activation temperature of 5°C
32 is typical of many residential smoke alarms. The propagated uncertainty of this estimate is
33 difficult to determine because temperature rise is not particularly well correlated with smoke
34 concentration within the sensing chamber of the detector. Nevertheless, the relative standard
35 deviation of the normalized activation times⁴ for the NIST Home Smoke-Alarm Experiments
36 is 34 percent. Without more detailed information about the activation criteria, the models cannot
37 predict the activation times more accurately than this value.

⁴ To determine this value, the activation times of multiple detectors at the same location were averaged and the activation times were normalized by the average value. Then, the standard deviation of the normalized activation times was calculated to produce the relative standard deviation of 34 percent.

3.3.3 Summary of Experimental Uncertainty Estimates

Table 3-4 summarizes the estimated uncertainties for all of the output quantities for which the models are to be evaluated. The rightmost column in the table represents the total experimental uncertainty, denoted as $\tilde{\sigma}_E$, a combination of the uncertainty in the measurement of the output quantity itself, along with the propagated uncertainties of the key measured input quantities. This total experimental uncertainty is obtained by taking the square root of the sum of the squares of the measurement and propagation uncertainties that have been estimated in the previous two subsections. It is assumed that the two forms of uncertainty are independent.

Table 3-4. Summary of the experimental uncertainty estimates.

Measured/Predicted Quantity	Measurement Uncertainty (%)	Key Input Parameters; Corresponding Relative Uncertainty (%); Power Dependence			Input Parameter Propagation Uncertainty (%)	Total Experimental Uncertainty, $\tilde{\sigma}_E$ (%)
HGL, Plume, Ceiling Jet, Surface, and Target Temperatures	5	HRR	7.5	2/3	5	7
HGL Depth	5	Door Height	0	-1	0	5
Gas Concentration	2	HRR	7.5	1	7.5	8
Smoke Concentration	14	HRR Soot Yield	7.5 11	1 1	13	19
Pressure	1	HRR Leak Area Vent. Rate	7.5 3.5 10	2 -2 2	21	21
Heat Flux	5	HRR Rad. Frac.	7.5 8	1 1	10	11
Sprinkler Activation Time	0	HRR RTI Act. Temp.	7.5 11 5	2/3 1 1	6	6
Cable Failure Time	0	Temp. Diameter Thickness	2.5 0.6 6.7	-	12	12
Smoke Detector Activation Time	0	Response Mechanism	-	-	34	34

4

MODEL DESCRIPTIONS

Numerous fire models have been developed and maintained by various organizations to predict fire-generated conditions. This study selects the following five of these fire models, which represent a wide range of capabilities and mathematical and computational sophistication:

1. NRC's Fire Dynamics Tools (FDT^s Version 1805.1)
2. EPRI's Fire-Induced Vulnerability Evaluation (FIVE-Rev2)
3. NIST's Consolidated Model of Fire Growth and Smoke Transport (CFAST Version 6.3.1)
4. EdF's MAGIC (Version 4.1.3)
5. NIST's Fire Dynamics Simulator (FDS Version 6.0.0)

These particular models were chosen based on the fact that most of them (a) have been used to calculate fire conditions in NPP fire protection applications or (b) were developed by stakeholders within the nuclear industry for NPP fire protection applications.

The results of the model validation study presented in Chapter 5 are based on these particular versions of the models. The validation results do not apply to earlier versions of the models.

4.1 Empirical Correlations: FDT^s and FIVE

The FDT^s are a set of empirical correlations in the form of Microsoft[®] Excel[®] spreadsheets. For the most part, the correlations in the FDT^s library are closed-form algebraic expressions programmed in spreadsheets to provide a user-friendly interface that reduces input and computational errors. Technical details are available in NUREG-1805 and in Supplement 1 to NUREG-1805. In addition to describing corrections and improvements of the original FDT^s spreadsheets, the supplement documents the implementation of the Thermally Induced Failure (THIEF) model for electrical cables (Volume 3 of NUREG/CR-6931, 2007) as Chapter 19.

FIVE is another library of engineering calculations in the form of Excel[®] spreadsheets. FIVE consists of functions programmed in Visual Basic, the programming language within Excel[®]. Technical details are available in EPRI 3002000830. To verify that the correlations work as programmed, the FDT^s and FIVE have been checked according to the verification cases listed in NIST SP 1169 (2013).

HGL Temperature, Natural Ventilation

For a compartment with natural ventilation, the correlation of McCaffrey, Quintiere, and Harkleroad (MQH) (Walton, 2008) predicts the HGL temperature rise.

HGL Temperature, Forced Ventilation

For a compartment with forced ventilation, the correlation of Foote, Pagni, and Alvares (FPA) or the correlation of Deal and Beyler (DB) (Walton, 2008) predicts the HGL temperature rise.

MODEL DESCRIPTIONS

1 **HGL Temperature, No Ventilation**

2 For a compartment with no ventilation, the correlation of Beyler (Walton, 2008) predicts the HGL
3 temperature rise.

4 **HGL Depth**

5 For a compartment with no ventilation and constant HRR, the available safe egress time (ASET)
6 correlation (Walton, 1985; Milke, 2008) predicts the HGL interface height. An alternative method
7 is presented by Yamana and Tanaka (Tanaka, 1985).

8 **Plume Temperature**

9 Correlations by Heskestad (2008) and McCaffrey (1979) estimate the increase in the centerline
10 plume temperature.

11 **Cable Failure Time**

12 The Thermally Induced Electrical Failure (THIEF) of a cable can be predicted using a simple
13 one-dimensional heat transfer calculation, under the assumption that the cable can be treated
14 as a homogeneous cylinder (NUREG/CR-6931, 2007). Cable failure is assumed when the cable
15 temperature exceeds an empirically determined critical temperature.

16 **Steel Temperature**

17 The temperature rise of an unprotected or protected steel member exposed to fire can be
18 predicted using heat transfer analysis on the steel member (Milke, 2008). There are different
19 formulations for unprotected steel and protected steel (both neglecting and accounting for the
20 thermal capacity of the insulation layer).

21 **Point Source Radiation Heat Flux**

22 The point source radiation model assumes that radiative energy is concentrated at a point
23 located within a flame (Beyler, 2008) and can be used to calculate the radiation heat flux on a
24 target or surface.

25 **Solid Flame Radiation Heat Flux**

26 The solid flame radiation model predicts the heat flux to a target based on the effective emissive
27 power from a flame and a view factor calculation (Beyler, 2008).

28 **Ceiling Jet Temperature**

29 For a steady-state fire, the correlation of Alpert (2008) predicts the ceiling jet temperature rise
30 from a fire plume.

31 **Sprinkler Activation Time**

32 For a steady-state fire, the correlation of Alpert (2008) along with a heat transfer analysis on the
33 sprinkler link (Budnick, Evans, and Nelson, 1997) can be used to predict the activation time of a
34 sprinkler.

35 **Smoke Detector Activation Time**

36 Smoke detector activation time is sometimes modeled in the same way as the activation time of
37 a sprinkler with a low activation temperature and RTI. Heskestad and Delichatsios (1977)
38 correlated smoke detector activation to a particular temperature rise that depends on the type of
39 fuel.

40

4.2 Zone Fire Models: CFAST and MAGIC

This section provides qualitative background information on two zone-fire models included in the V&V study, CFAST and MAGIC, including their development and use. Zone-fire models (also referred to as two-zone models) are modeling programs developed under the assumption that a fire will generate two distinct zones with uniform thermal properties.

4.2.1 Basic Description of Zone Fire Models

Zone fire models such as CFAST and MAGIC predict the fire induced environment as a function of time for single- or multi-compartment scenarios. Each compartment is divided into two zones (or volumes) in order to numerically solve differential equations, and the two volumes are assumed to be uniform in temperature and species concentration. The approximate solution of the conservation equations for each zone, together with the ideal gas law and the equation of heat conduction into the walls, is used in attempts to simulate the environmental conditions generated by a fire.

CFAST (Peacock et al., 2013) is a two zone fire model that predicts the environment that arises within compartments as a result of a fire prescribed by the user. CFAST was developed and is maintained by NIST's Fire Research Division. CFAST predicts the average temperatures of the upper and lower gas layers within each compartment; flame height; ceiling, wall, and floor temperatures within each compartment; flow through vents and openings; visible smoke and gas species concentrations within each layer; target temperatures; heat transfer to targets; sprinkler activation time; and the impact of sprinklers on the fire's HRR. Version 6.3.1 was used for the current study.

MAGIC (Gay et al. 2012b) is a two-zone fire model developed and maintained by EdF. It is available through EPRI to its members. In terms of modeling capabilities, MAGIC predicts (1) environmental conditions in the room (such as hot gas layer temperature and oxygen/smoke concentrations), (2) heat transfer-related outputs to walls and targets (such as incident, convective, radiated, and total heat fluxes), (3) fire intensity and flame height, and (4) flow velocities through vents and openings. Version 4.1.3 was used for the current study.

The models use similar, but not identical assumptions, governing equations, and engineering correlations. Significant similarities and differences are highlighted in the sections that follow.

4.2.2 Developers of Zone Fire Models

The CFAST model was developed, and is maintained, by the Fire Research Division of NIST. The developers include Walter Jones, Richard Peacock, Glenn Forney, Rebecca Portier, Paul Reneke, John Hoover, and John Klote.

MAGIC was developed and is maintained by Electricité de France (EdF).

4.2.3 Documentation of Zone Fire Models

Relevant publications concerning CFAST include the CFAST Technical Reference Guide (Peacock et al., 2013), User's Guide (Peacock et al., 2013a), and Model Evaluation Guide (Peacock et al., 2013b). The Technical Reference Guide describes the underlying physical principles, provides a comparison with experimental data, and describes the limitations of the model. The User's Guide describes how to use the model.

MODEL DESCRIPTIONS

1 MAGIC is supported by three EdF publications, including (1) the technical manual, which
2 provides a mathematical description of the model (Gay and Wizenne 2012b); (2) the user's
3 manual, which details how to use the graphical interface (Gay and Wizenne 2012a); and (3) the
4 validation studies, which compare MAGIC's results with experimental measurements (Gay and
5 Wizenne 2012c). These three proprietary publications are available through EPRI to EPRI
6 members.

7 **4.2.4 Governing Equations and Assumptions for Zone Fire Models**

8 The general equations solved by both CFAST and MAGIC include conservation of mass and
9 energy. The models do not explicitly solve the momentum equation, except for use of the
10 Bernoulli equation for the flow velocity at vents. These equations and the ideal gas law are
11 solved to obtain fire-generated conditions in the selected control volumes.

12 Zone models are implemented based on two general assumptions: (1) two zones per
13 compartment provide a reasonable approximation of the scenario being evaluated, and (2) the
14 complete momentum equation is not needed to solve the set of equations associated with the
15 model. Consequently, the two zones have uniform properties. That is, the temperature and gas
16 concentrations are assumed to be constant throughout the zone; the properties only change as
17 a function of time.

18 Chapter 3 of the CFAST Technical Reference Guide (Peacock et al., 2013) fully describes the
19 equations and assumptions associated with the CFAST model. A complete technical description
20 of the MAGIC algorithms and sub-models is provided in the MAGIC documentation (Gay and
21 Wizenne, 2012).

22 **4.2.5 Input Data for Zone Fire Models**

23 All of the data required to run a zone model (CFAST or MAGIC) reside in a primary data file, which
24 the user creates. Some instances might require databases of information on objects,
25 thermophysical properties of boundaries, and sample prescribed fire descriptions. In general,
26 the data files contain the following information:

- 27 • Compartment dimensions (height, width, and length). The compartment (or each
28 compartment in a multi-room scenario) is assumed to have a rectangular floor base and
29 flat ceiling.
- 30 • Construction materials of the compartment (e.g., concrete and gypsum), including
31 material properties (e.g., thermal conductivity, specific heat, density, thickness, and heat of
32 combustion). Depending on the selected material, this information might be available in
33 databases supplied by the model developers.
- 34 • Dimensions and positions of horizontal and vertical flow openings such as doors,
35 windows, vents, and leakage paths.
- 36 • Mechanical ventilation specifications (injection and extraction rates, vent elevations, and
37 time to start/stop the system).
- 38 • Fire properties (e.g., heat-release rate, heat of combustion, lower oxygen limit,
39 species-production rates as a function of time, radiative fraction, and fuel composition).
- 40 • Fire location (lateral position, elevation, and position relative to a wall or corner).
- 41 • Footprint area of the fire: For CFAST, this is specified as an area of no particular shape.
42 For MAGIC, the specification includes whether the fire is circular in shape (e.g., pool
43 fires specified by the diameter) or rectangular (e.g., bounded pool fires or fires in
44 electrical cabinets specified by length and width).

- Sprinklers and detectors are characterized by their location within the compartment and their response characteristics, which include activation temperature and response-time index.
- Two sets of parameters (thermophysical properties and location) describe targets. Thermophysical properties include the density, specific heat, and thermal conductivity of the material. Location refers to where the target is with respect to the fire (expressed with three-dimensional coordinates).

Many of these properties are commonly available in fire protection engineering and materials handbooks. Experimentally determined property data might also be available for certain scenarios. However, depending on the application, properties for specific materials might not be readily available. A small file distributed with the CFAST and MAGIC software contains a database with thermal properties of common materials. These data are given as examples; users should verify the accuracy and appropriateness of the data.

The CFAST User's Guide (Peacock et al., 2013a) provides a complete description of the required input parameters. Some of these parameters have default values included in the model, which are intended to be representative for a range of fire scenarios. Unless explicitly noted, default values were used for parameters not specifically included in this validation study.

The MAGIC User's Guide (Gay and Wizenne, 2012a) provides a complete description of the input parameters required to run MAGIC.

4.2.6 Output Quantities of Zone-Fire Models

Once the simulation is complete, CFAST produces an output file containing all of the solution variables. Typical outputs include (but are not limited to) the following:

- environmental conditions in the room (such as hot gas layer temperature; oxygen and smoke concentration; and ceiling, wall, and floor temperatures)
- heat transfer related outputs to walls and targets (such as incident, convective, radiated, and total heat fluxes)
- fire intensity and flame height
- flow velocities through vents and openings
- sprinkler activation time

MAGIC has an extensive library of output values. Once a given simulation is completed, MAGIC generates an output file with all of the solution variables. Through a "post-processor" interface, the user selects the relevant output variables for the analysis. Typical outputs include (but are not limited to) the following examples:

- environmental conditions in the room (such as hot gas layer temperature, oxygen concentration, and smoke concentration)
- heat transfer related outputs to wall and targets (such as incident, convective, radiated, and total heat fluxes)
- oxygen effects on heat-release rate and flame height
- flow velocities through vents and openings
- target temperatures (including sprinkler bulb temperature and gas temperature measured by the detectors)

MODEL DESCRIPTIONS

1 **4.2.7 Verification of Zone-Fire Models**

2 This section documents the mathematical and numerical robustness of CFAST and MAGIC,
3 which involves verifying that the implementation of the model matches the stated
4 documentation. Specifically, ASTM E1355 suggests the following analyses to address the
5 mathematical and numerical robustness of models:

- 6 • Analytical tests involve testing the correct functioning of the model. In other words, these
7 tests use the code to solve a problem with a known mathematical solution. However,
8 there are relatively few situations for which analytical solutions are known.
9
- 10 • “Code checking” refers to verifying the computer code on a structural basis. This
11 verification can be achieved manually or by using a code-checking program to detect
12 irregularities and inconsistencies within the computer code.
13
- 14 • Numerical tests investigate the magnitude of the residuals from the solution of a
15 numerically solved system of equations (as an indicator of numerical accuracy) and the
16 reduction in residuals (as an indicator of numerical convergence).

17 **Analytical Tests:** General analytical solutions do not exist for most fire problems. Nonetheless,
18 it is possible to test specific aspects of the model in typical situations.

19 Certain CFAST sub-models address phenomena that have analytical solutions; for example,
20 one-dimensional heat conduction through a solid or pressure increase in a sealed or slightly
21 leaky compartment as a result of a fire or fan. The developers of CFAST routinely use analytical
22 solutions to test sub-models to verify the correctness of the coding of the model as part of its
23 development. Such routine verification efforts are relatively simple and the results might not
24 always be published or included in the documentation. Two additional types of verification are
25 possible. The first type involves validating individual algorithms against experimental work. The
26 second involves simple experiments, especially for conduction and radiation, for which the
27 results are asymptotic (e.g., for a simple single-compartment test case with no fire, all
28 temperatures should equilibrate asymptotically to a single value). Such comparisons are
29 included in the CFAST model evaluation guide (Peacock et al., 2013b).

30 Some studies have been performed to control the correct behavior of the following sub-models
31 of MAGIC:

- 32 • conduction into the wall: comparison to other models and analytic solutions
33
- 34 • target and cable thermal behavior: consistency of the behavior in typical situations
35
- 36 • plumes model: comparison with the theoretical model
37
- 38 • vent and opening: comparison to other zone and field models
39
- 40 • room pressure: comparison with pressure estimated by the perfect gas law and
41 simplified energy equation

42 These studies are EdF’s proprietary material.

1 Code Checking:

2 Standard programs have been used to check the CFAST model structure and language.
3 Specifically, FLINT, LINT, and Forcheck have been applied to the entire model to verify the
4 correctness of the interface, undefined or incorrectly defined (or used) variables and constants,
5 and completeness of loops and threads.

6 The CFAST code has also been checked by compiling and running the model on a variety of
7 computer platforms. Because FORTRAN and C are implemented differently for various
8 computers, this represents both a numerical check as well as a syntactic check. CFAST has
9 been compiled for the Sun[®] (Solaris), SGI[®] (IRIX[®]), and Concurrent computer platforms, as well
10 as PCs running Microsoft Windows[®] (Lahey, Digital (Compaq[®]), and Intel[®] FORTRAN). Within
11 the precision afforded by the various hardware implementations, the answers are identical.⁵

12 The source code for MAGIC is tested with the following methods:

13 • First, to control robustness, the code may be compiled in several different platforms and
14 software applications. The MAGIC code has been compiled under Microsoft
15 Windows 2000, Windows XP, Windows Vista, and Windows 7, with a variety of
16 compilers, including Absoft[®] Pro FORTRAN, Visual FORTRAN, and G77 (gfortran). In
17 addition, a global update of the FORTRAN sources was performed in 2004
18 (Benmamoun, 2004), and aspects such as code documentation, variable glossary, and
19 source cleanup were addressed.

20 • In terms of code quality, two tools have been used to control the language:

- 21 ○ FOR_STUDY[®] from Cobalt Blue
- 22 ○ *plusFORT* from Polyhedron Software

23 These tools confirm the consistency of variables and constants (undefined and
24 incorrectly or redundantly declared) and use of good FORTRAN syntax.

25 The software quality-assurance system (Gautier, 1996) provides a process to fix detected
26 anomalies concerning the interface of the code. Maintenance of MAGIC is based on observation
27 forms, which identify problems; modification forms, which describe the problem analysis and
28 proposed solutions; and correction forms, which explain the chosen solution and implementation
29 features. The project manager decides on the implementation of the correction in future
30 versions.

31 **Numerical Tests:** Two components of the numerical solutions of CFAST must be verified. The
32 first is the differential-algebraic equation (DAE) solver called DASSL, which has been tested for
33 a variety of differential equations and is widely used and accepted (Barnett, 1990). The radiation
34 and conduction routines have also been tested against known solutions for asymptotic results.

35 The second component is the coupling between algorithms and the general solver. The
36 structure of CFAST provides close coupling that avoids most errors. The error attributable to
37 numerical solution is far less than that associated with the model assumptions. Also, CFAST is
38 designed to use 64-bit precision for real-number calculations to minimize the effects of
39 numerical error. CFAST includes a number of numerical tests in the CFAST Evaluation Guide
40 (Peacock et al., 2013b).

⁵ Typically, an error limit of one part in 10⁶.

MODEL DESCRIPTIONS

1 For each new MAGIC version, a set of tests is used to ensure that the calculation is correct.
2 These tests come from previous case studies. The convergence and speed of the calculation is
3 the first step of control. Main results from the original study are then compared, and significant
4 differences are analyzed. These studies are EdF proprietary material.

5 Specific tests are performed in the maintenance process when new models are implemented in
6 MAGIC or when existing models are corrected or improved. Those tests are not systematically
7 conducted for new versions, but they are available in case problems arise with the model under
8 study. The tests are mentioned in the correction report (Gautier, 1996) which is kept for each
9 code correction. These reports are EdF proprietary material and not published.

10 **4.2.8 Limitations of Zone Fire Models**

11 Zone models have been developed for use in solving practical fire problems in fire protection
12 engineering, while also providing a tool to study fundamental fire dynamics and smoke spread.
13 They are intended for use in system modeling of buildings and building components. They are
14 not intended for detailed study of flow within a compartment, such as is needed for detailed
15 smoke detector placement. Both CFAST and MAGIC include the activation of sprinklers and fire
16 suppression by water droplets.

17 The most extensive use of the models is for fire and smoke spread in complex buildings. Their
18 efficiency and computational speed are inherent in the few computation cells needed for the
19 implementation of a zone model. These models are used for the design and reconstruction of
20 timelines for fire and smoke spread in residential, commercial, and industrial fire applications.
21 Some applications of the models have been for design of smoke-control systems.

22 **Compartments:** Zone models are generally limited to situations in which the compartment
23 volumes are strongly stratified. However, in order to facilitate the use of the model for
24 preliminary estimates when a more sophisticated calculation is ultimately needed, there are
25 algorithms for corridor flow, smoke-detector activation, and detailed heat conduction through
26 solid boundaries. CFAST does permit modeling of non-rectangular compartments, although the
27 application is intended to be limited to relatively simple spaces. There is no intent to include
28 complex geometries in which a complex flow field is a driving force. For these applications,
29 computational fluid dynamics (CFD) models are appropriate.

30 **Gas Layers:** There are also limitations inherent in the assumption of stratification of the gas
31 layers. The zone model concept, by definition, implies a sharp boundary between the upper and
32 lower layers, whereas in reality the transition is typically over about 10 percent of the height of
33 the compartment and can be larger in weakly stratified flow. For example, a burning cigarette in
34 a normal room is not within the purview of a zone model. While it is possible to make predictions
35 within 5 percent of the actual temperatures of the gas layers, this is not the optimum use of the
36 model. It is more properly used to make estimates of fire spread (not flame spread), smoke
37 detection and contamination, and life safety calculations.

38 **Heat Release Rate:** There are limitations inherent in the assumptions used in the application of
39 the empirical models. As a general guideline, the heat release should not exceed about
40 1 MW/m^3 . This is a limitation on the numerical routines attributable to the coupling between gas
41 flow and heat transfer through boundaries (conduction, convection, and radiation). The inherent
42 two-layer assumption is likely to break down well before this limit is reached.

43 **Heat Transfer:** Both models include radiation, convection, and conduction sub-models that
44 include the interaction between the fire, gas layers, and compartment surfaces. MAGIC
45 additionally includes the impact of radiation through vents to other compartments or the

1 outdoors; CFAST does not include this effect. Both models include calculation of heat transfer to
2 user-placed targets within compartments.

3 **Ventilation and Leakage:** The vent flow algorithms in both CFAST and MAGIC assume that
4 the size of an individual vent is small compared to the total surface area of the connecting
5 compartments. With larger vents, some additional uncertainty in the calculated flows can be
6 expected. An important limitation arises from the uncertainty in the scenario specification. For
7 example, leakage in buildings is significant, and this affects flow calculations especially when
8 wind is present and for tall buildings. These effects can overwhelm limitations on accuracy of
9 the implementation of the model. The overall accuracy of the model is closely tied to the
10 specificity, care, and completeness with which the data are provided.

11 **Thermal Properties:** The accuracy of the model predictions is limited by how well the user can
12 specify the thermophysical properties. For example, the fraction of fuel which ends up as soot
13 has an important effect on the radiation absorption of the gas layer and, therefore, the relative
14 convective versus radiative heating of the layers and walls, which in turn affects the buoyancy
15 and flow. The level of uncertainty of the predictions is higher if the properties of real materials
16 and real fuels are unknown or difficult to obtain or if the physical processes of combustion,
17 radiation, and heat transfer are more complicated than their mathematical representations in a
18 zone model.

19 **4.3 CFD Fire Model: FDS**

20 This section contains information about the Fire Dynamics Simulator (FDS), its development,
21 and its use in fire-protection engineering. Most of the information has been extracted from the
22 FDS Technical Reference Guide (McGrattan et al., 2013), which contains a comprehensive
23 description of the governing equations and numerical algorithms used to solve them.

24 **4.3.1 FDS Basic Description**

25 FDS is a computational fluid dynamics (CFD) model of fire-driven fluid flow. The model
26 numerically solves a form of the Navier-Stokes equations appropriate for low-speed thermally
27 driven flow with an emphasis on smoke and heat transport from fires. The partial derivatives of
28 the conservation equations of mass, momentum, and energy are approximated as finite
29 differences and the solution is updated in time on a three-dimensional rectilinear grid. Thermal
30 radiation is computed using a finite volume technique on the same grid as the flow solver.
31 Lagrangian particles are used to simulate smoke movement and sprinkler sprays. Smokeview is
32 a companion program that produces images and animations of the FDS calculations.

33 Version 1 of FDS/Smokeview was publicly released in February 2000, The present version of
34 FDS/Smokeview is Version 6, which was released in September 2013. Changes in the version
35 number correspond to major changes in the physical model or input parameters. For minor
36 changes and bug fixes, incremental versions are released, cited according to fractions of the
37 integer version number. Version 6.0.0 was used for the current study.

38 **4.3.2 FDS Developers**

39 FDS was developed, and is currently maintained, by the Fire Research Division at NIST.
40 A substantial contribution to the development of the model was made by VTT Building and
41 Transport in Finland.

1 **4.3.3 FDS Documentation**

2 FDS is documented by two publications, the Technical Reference Guide
3 (McGrattan et al., 2013) and the FDS User's Guide (McGrattan et al., 2013b). The FDS User's
4 Guide describes how to use the model. The Technical Reference Guide consists of four
5 volumes. Volume 1 discusses the mathematical formulation of the model. Volume 2 documents
6 the verification of the model algorithms. Volume 3 documents the validation of the model.
7 Volume 4 is the configuration-management plan; that is, the process of model development and
8 maintenance.

9 NIST has developed a public Web site to distribute FDS and Smokeview and support users of
10 the programs. The web site (<http://fire.nist.gov/fds/>) also includes documents that describe
11 various parts of the model in detail.

12 **4.3.4 FDS Governing Equations and Assumptions**

13 **Hydrodynamic Model:** FDS numerically solves a form of the Navier-Stokes equations
14 appropriate for low-speed thermally driven flow with an emphasis on smoke and heat transport
15 from fires. The core algorithm is an explicit predictor-corrector scheme and is second-order
16 accurate in space and time. Turbulence is treated by means of large eddy simulation (LES). It is
17 possible to perform a direct numerical simulation (DNS) if the underlying numerical grid is fine
18 enough.

19 **Combustion Model:** For most applications, FDS assumes that combustion is mixing-controlled
20 and that the reaction of fuel and oxygen is infinitely fast.

21 **Radiation:** Radiation heat transfer is included in the model through the solution of the radiation
22 transport equation for a non-scattering gray gas. In a limited number of cases, a wideband
23 model can be used in place of the gray gas model. The radiation equation is solved using a
24 technique similar to a finite volume method for convective transport, so the name given to it is
25 "the finite volume method."

26 **Geometry:** FDS approximates the governing equations on one or more rectilinear grids. The
27 user prescribes rectangular obstructions that are forced to conform to the underlying grid.

28 **Boundary Conditions:** All solid surfaces are assigned thermal boundary conditions, as well as
29 information about the burning behavior of the material. Usually, material properties are stored in
30 a database and invoked by name. Heat and mass transfer to and from solid surfaces is usually
31 handled with empirical correlations.

32 **Sprinklers and Detectors:** The activation of sprinklers and heat and smoke detectors is
33 modeled using fairly simple correlations based on thermal inertia (in the case of sprinklers and
34 heat detectors) and the lag in smoke transport through smoke detectors. Sprinkler sprays are
35 modeled by Lagrangian particles that represent a sampling of the water droplets ejected from
36 the sprinkler.

37 **4.3.5 FDS Input Data**

38 All of the input parameters required by FDS to describe a particular scenario are conveyed in
39 one text file created by the user. This file contains information about the numerical grid, ambient
40 environment, building geometry, material properties, combustion kinetics, and desired output
41 quantities. The numerical grid is one or more rectilinear meshes with (usually) uniform cells. All
42 geometric features of the scenario have to conform to this numerical grid. An obstruction that is

1 smaller than a single grid cell is either approximated as a single cell or rejected. The building
2 geometry is input as a series of rectangular obstructions. Materials are defined by their thermal
3 conductivity, specific heat, density, thickness, and burning behavior. This information is
4 conveyed in various ways depending on the desired level of detail. A significant part of the FDS
5 input file directs the code to output various quantities in various ways. Much as in an actual
6 experiment, the user must decide before the calculation begins what information to save. There
7 is no way to recover information after the calculation is over if it was not requested at the start.
8 A complete description of the input parameters required by FDS can be found in the FDS User's
9 Guide (McGrattan et al., 2013b).

10 A number of material properties are needed as inputs for FDS, most related either to solid
11 objects or the fuel. In many fire scenarios, the solid objects are the fuel. For solid surfaces, FDS
12 needs the density, thermal conductivity, specific heat, and emissivity. Note that FDS does not
13 distinguish between walls and various other solid objects, sometimes regarded as "targets" in
14 simpler models.

15 For the fuel, FDS needs to know whether it is a solid, liquid, or gas; its heat of combustion; its
16 heat of vaporization (liquids and solids); the stoichiometric coefficients of the ideal reaction; the
17 soot and carbon monoxide (CO) yields; and the fraction of energy released in the form of
18 thermal radiation. The radiative fraction is not an inherent property of the fuel, but rather a
19 measured quantity that varies with the size and geometric configuration of the fire. It can be
20 computed directly by FDS, but it is often input directly because it cannot be predicted reliably
21 with the present form of the combustion model.

22 Some of the property data needed by FDS are commonly available in fire-protection engineering
23 and materials handbooks. Depending on the application, properties for specific materials might
24 not be readily available (especially burning behavior at different heat fluxes). A small file
25 distributed with the FDS software contains a database with thermal properties of common
26 materials. These data are given as examples; users should verify the accuracy and
27 appropriateness of the data.

28 **4.3.6 FDS Output Quantities**

29 FDS computes the temperature, density, pressure, velocity, and chemical composition within
30 each numerical grid cell at each discrete time step. There are typically hundreds of thousands to
31 several million grid cells and thousands to hundreds of thousands of time steps. In addition,
32 FDS computes at solid surfaces the temperature, heat flux, mass-loss rate, and various other
33 quantities. Typical output for the gas phase includes the following quantities:

- 34 • gas temperature
- 35 • gas velocity
- 36 • gas species concentration (water vapor, carbon dioxide (CO₂), CO, and nitrogen (N₂))
- 37 • smoke concentration and visibility estimates
- 38 • pressure
- 39 • heat release rate per unit volume
- 40 • mixture fraction (or air/fuel ratio)
- 41 • gas density
- 42 • water droplet mass per unit volume

MODEL DESCRIPTIONS

1 On solid surfaces, FDS predicts additional quantities associated with the energy balance
2 between gas and solid phases, including the following examples:

- 3 • surface and interior temperature
- 4 • heat flux, both radiative and convective
- 5 • burning rate
- 6 • water droplet mass per unit area

7 In addition, the program records the following global quantities:

- 8 • total heat release rate (HRR)
- 9 • sprinkler and detector activation times
- 10 • mass and energy fluxes through openings or solids

11 Time histories of various quantities at a single point in space or global quantities such as the
12 fire's heat-release rate (HRR) are saved in simple comma-delimited text files that can be plotted
13 using a spreadsheet program. However, most field or surface data are visualized with a
14 program called Smokeview, a tool specifically designed to analyze data generated by FDS.

15 **4.3.7 FDS Verification**

16 The verification of FDS is documented in Volume 2 of the FDS Technical Reference Guide
17 (McGrattan et al., 2013). This document describes a set of several hundred test cases that fall
18 into three basic categories:

19 **Analytical Tests:** These involve comparison of the computed solutions with closed-form
20 solutions of the governing equations. There are no closed-form mathematical solutions for the
21 fully turbulent, time-dependent Navier-Stokes equations. CFD provides an approximate solution
22 for the nonlinear partial differential equations by replacing them with discretized algebraic
23 equations that can be solved using a powerful computer. Certain sub-models address
24 phenomena that have analytical solutions. The developers of FDS routinely use analytical
25 solutions to test sub-models to verify the correctness of the coding of the model. With each new
26 release of FDS, the entire set of verification calculations is run to ensure that no new errors
27 have been introduced into the source code. Some of these include the following examples:

- 28 • heat conduction into a semi-infinite solid
- 29 • evaporation of water droplets in uniform temperature environment
- 30 • radiation heat transfer from a hot object with a uniform temperature
- 31 • pressure increase in a sealed or slightly leaky compartment attributable to a fire or fan
- 32 • idealized reaction of fuel and oxygen in an adiabatic chamber

33 The common thread in all of these exercises is the well-defined initial and final states, which test
34 the basic conservation laws.

35 **Code Checking:** This involves verification of the basic structure of the computer code, either
36 manually or automatically with a code-checking program, to detect irregularities and
37 inconsistencies. FDS has been compiled and run on computers manufactured by several
38 companies and run under various operating systems, including Unix, Linux, Microsoft Windows,
39 and Apple® OS X®. Various Fortran compilers have been used as well. Each combination of
40 hardware, operating system, and compiler involves a slightly different set of compiler and
41 run-time options. Compliance with the Fortran standard of the International Organization for
42 Standardization (ISO) and American National Standards Institute (ANSI) improves the portability
43 of the program. By adhering to the standard, the code is streamlined and outdated or potentially

1 harmful code is removed. FDS version 6 is fully compliant with the Fortran 2003 ISO/ANSI
2 standard.

3 **Numerical Tests:** These involve assessment of the magnitude of the residuals from the
4 solution of a numerically solved system of equations (as an indicator of numerical accuracy) and
5 the reduction in residuals (as an indicator of numerical convergence). The use of finite
6 differences to approximate spatial and temporal partial derivatives introduces error into the FDS
7 calculation. This numerical error depends on the grid size. As the numerical grid is refined, the
8 numerical error decreases. If the grid is refined to about 1 mm or less, the simulation becomes a
9 direct numerical simulation (DNS), where no assumptions about the underlying turbulence need
10 to be made. While DNS simulations are too costly for practical fire calculations, they can be
11 useful in checking the numerical algorithm because there exist in the literature a variety of
12 small-scale fluid flow and combustion experiments that can be simulated in great detail.
13 Numerous comparisons between small-scale experiments and DNS solutions using FDS have
14 shown that the hydrodynamic solver is robust and without serious flaws.

15 **4.3.8 FDS Limitations**

16 Although FDS can address most fire scenarios, there are limitations in all of its various
17 algorithms. Some of the more prominent limitations of the model are listed here. More specific
18 limitations are discussed as part of the description of the governing equations in the FDS
19 Technical Reference Guide (McGrattan et al., 2013).

20 **Low-Speed Flow Assumption:** The use of FDS is limited to low-speed flow (having a Mach
21 number less than about 0.3) with an emphasis on smoke and heat transport from fires. This
22 assumption rules out using the model for any scenario involving flow speeds approaching the
23 speed of sound, such as explosions, choke flow at nozzles, and detonations.

24 **Rectilinear Geometry:** The efficiency of FDS is attributable to the simplicity of its rectilinear
25 numerical grid and the use of fast, direct solvers for the pressure field. This can be a limitation in
26 some situations in which certain geometric features do not conform to the rectangular grid,
27 although most building components do. For most practical large-scale simulations, the
28 increased grid resolution afforded by the fast pressure solver offsets the approximation of a
29 curved boundary by small rectangular grid cells.

30 **Fire Growth and Spread:** FDS was originally intended for design scenarios in which the heat
31 release rate of the fire is specified and the transport of heat and exhaust products is the
32 principal aim of the simulation. However, for fire scenarios in which the heat release rate is
33 predicted rather than prescribed, the uncertainty of the model is higher. There are several
34 reasons for this: (1) properties of real materials and real fuels are often unknown or difficult to
35 obtain; (2) the physical processes of combustion, radiation, and solid-phase heat transfer are
36 more complicated than their mathematical representations in FDS; and (3) the results of
37 calculations are sensitive to both the numerical and physical parameters.

38 **Combustion:** For most applications, FDS assumes that combustion is mixing-controlled and
39 that the reaction of fuel and oxygen is infinitely fast, regardless of the temperature. For
40 large-scale well-ventilated fires, this is a good assumption. However, if a fire is in an
41 under-ventilated compartment, or if a suppression agent such as water mist or CO₂ is
42 introduced, fuel and oxygen might mix but might not burn. Also, a shear layer with high strain
43 rate separating the fuel stream from an oxygen supply can prevent combustion from taking
44 place. The physical mechanisms underlying these phenomena are complex, and even simplified
45 models still rely on an accurate prediction of the flame temperature and local strain rate.

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1 Sub-grid scale modeling of gas phase suppression and extinction is still an area of active
2 research in the combustion community. Until reliable models can be developed for
3 building-scale fire simulations, simple empirical rules can be used that prevent burning from
4 taking place when the atmosphere immediately surrounding the fire cannot sustain the
5 combustion.

6 **Radiation:** Radiative heat transfer is included in the model through the solution of the radiation
7 transport equation for a non-scattering gray gas and (in some limited cases) through using a
8 wideband model. The equation is solved using a technique similar to finite volume methods for
9 convective transport; thus, the name given to it is “the finite volume method.” The model has
10 several limitations. First, the absorption coefficient for the smoke-laden gas is a complex
11 function of its composition and temperature. Because of the simplified combustion model, the
12 chemical composition of the smoky gases, especially the soot content, can affect both the
13 absorption and emission of thermal radiation. Second, the radiation transport is discretized
14 through approximately 100 solid angles. For targets far away from a localized source of
15 radiation, like a growing fire, the discretization can lead to a non-uniform distribution of the
16 radiant energy. This can be seen in the visualization of surface temperatures, where “hot spots”
17 show the effect of the finite number of solid angles. The problem can be lessened by the
18 inclusion of more solid angles, but at a price of longer computing times. In most cases, the
19 radiative flux to far-field targets is not as important as those in the near-field, where coverage by
20 the default number of angles is much better.

21

5

VALIDATION RESULTS

This chapter describes the results of the validation study, including a description of the metrics used to quantify the model uncertainty.

5.1 Model Uncertainty Metrics

The accuracy of each model in predicting a particular quantity is summarized with a scatter plot like the one shown in Figure 5-1. The measured values are represented by the horizontal axis and the predicted values by the vertical. If a particular prediction and measurement are the same, the resulting point falls on the solid diagonal line. To better make use of these results, two statistical parameters are calculated for each model and each predicted quantity. The first parameter, δ , is the *bias factor*. It indicates the extent to which the model, on average, under- or overpredicts the measurements of a given quantity. For example, the bias factor for the data shown in Figure 5-1 is 0.98. This means that the model has been shown to slightly underestimate the ceiling-jet temperatures by 2 percent, on average, and this is shown graphically by the red line just below the diagonal. The second parameter is the *relative standard deviation* of the model, $\tilde{\sigma}_M$. This indicates the variability of the model. Referring again to Figure 5-1, there are two sets of off-diagonal lines. The first set, shown as dashed black lines, indicate the uncertainty of the experimental measurements in terms of a relative standard deviation, $\tilde{\sigma}_E$. It is assumed that the experiments are unbiased; that is, the bias factor for the experimental measurements is 1. The slopes of the dashed black lines are $1 \pm 2\tilde{\sigma}_E$, representing the 95 percent confidence intervals. The set of red dashed lines indicate the model's relative standard deviation, $\tilde{\sigma}_M$. The slopes of these lines are $\delta \pm 2\tilde{\sigma}_M$. If the model were as accurate as the measurements against which it is compared, the two sets of off-diagonal lines would merge. The extent to which the data scatters outside the experimental bounds is an indication of the degree of model uncertainty.

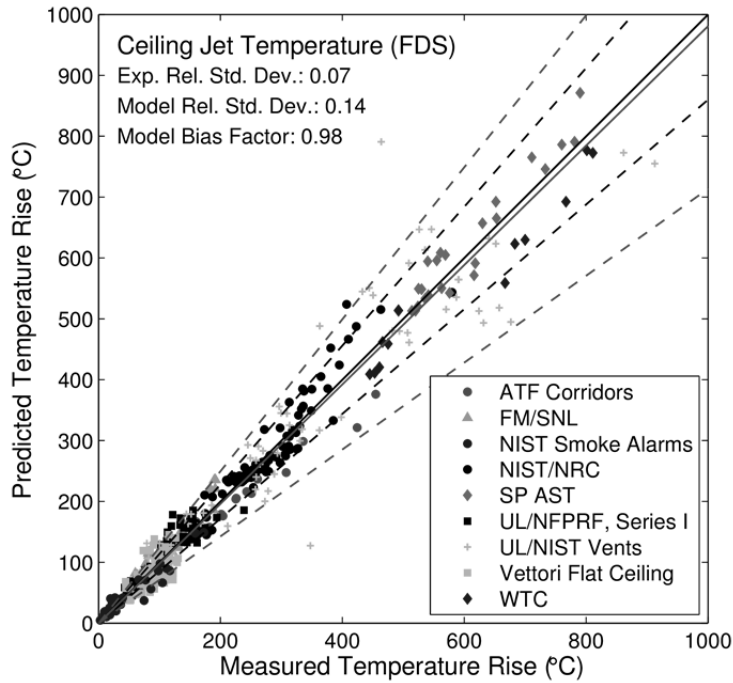
The derivation of the relevant uncertainty statistics has previously been presented by McGrattan and Toman (2011) and is summarized here. The calculation of δ and $\tilde{\sigma}_M$ uses a weighted⁶ set of measured and predicted values, along with an estimate of the experimental relative standard deviation, $\tilde{\sigma}_E$, derived in Section 3.3. Before describing the calculation, a few assumptions must be made:

1. The experimental measurements are assumed to be unbiased, and their uncertainty is assumed to be normally distributed with a constant relative standard deviation $\tilde{\sigma}_E$. The experimental uncertainty is a combination of the uncertainty in the measurement of the given quantity and the uncertainty of various important input parameters propagated

⁶ Referring to Figure 5-1, data points are often unevenly distributed over the range of the quantity of interest. For example, dozens of temperatures might be measured in the interval from 0°C to 100°C, while only a few are measured in the interval from 900°C to 1000°C. To correct for this when computing the bias and standard deviation, the data is weighted so that points in a sparsely covered interval are of equal value to the points in a densely covered interval. The entire range (in this case, 0°C to 1000°C) is divided into 10 equal intervals. The data from each interval is weighted so that each interval has equal weight in computing the accuracy metrics.

VALIDATION RESULTS

- 1 through the model. Table 5-1 provides estimates of relative experimental uncertainties for
 2 the quantities of interest.
- 3 2. The true value of the quantity of interest is assumed to be normally distributed about the
 4 predicted value divided by a bias factor δ . The relative standard deviation of the distribution
 5 is denoted as $\tilde{\sigma}_M$.



6
 7 **Figure 5-1. Sample result from validation study.**

- 8 The computation of the estimated bias and scatter associated with model error proceeds as
 9 follows. Given a set of n experimental measurements, E_i , and a corresponding set of model
 10 predictions, M_i , compute the following:

$$\overline{\ln(M/E)} = \frac{1}{n} \sum_{i=1}^n \ln(M_i/E_i) \quad (5-1)$$

- 11 The standard deviation of the model error $\tilde{\sigma}_M$ can be computed from the following equation:

$$\sqrt{\tilde{\sigma}_M^2 + \tilde{\sigma}_E^2} \cong \sqrt{\frac{1}{n-1} \sum_{i=1}^n [\ln(M_i/E_i) - \overline{\ln(M/E)}]^2} \quad (5-2)$$

- 12 The bias factor is:

$$\delta = \exp\left(\overline{\ln(M/E)} + \frac{\tilde{\sigma}_M^2 - \tilde{\sigma}_E^2}{2}\right) \quad (5-3)$$

- 1 For a given model prediction M , the “true” value of the quantity of interest is assumed to be a
 2 normally distributed random variable with a mean value of $\mu = M/\delta$ and a standard deviation of
 3 $\sigma = \tilde{\sigma}_M(M/\delta)$.
 4 Using these values, the probability of exceeding a critical value x_c is:

$$P(x > x_c) = \frac{1}{2} \operatorname{erfc}\left(\frac{x_c - \mu}{\sigma\sqrt{2}}\right) \quad (5-4)$$

- 5 Note that the *complimentary error function* is defined as follows:

$$\operatorname{erfc}(x) = \frac{2}{\sqrt{\pi}} \int_x^{\infty} e^{-t^2} dt \quad (5-5)$$

- 6 It is a standard function in mathematical or spreadsheet programs such as Microsoft Excel⁷.

7 **5.1.1 Example**

- 8 As an example of how to use the uncertainty metrics, consider the following example. Suppose
 9 that electrical cables within a compartment are assumed to fail if their surface temperature
 10 reaches 330°C (626°F). Suppose also that the CFD model FDS predicts that the maximum
 11 cable temperature caused by a fire within the compartment is 300°C (572°F). What is the
 12 probability that the cables could fail?

- 13 Step 1: Subtract the ambient value of the cable temperature, 20°C (68°F), to determine the
 14 predicted temperature rise. Refer to this value as the *model prediction*, M :

$$M = 300 \text{ °C} - 20 \text{ °C} = 280 \text{ °C} \quad (5-6)$$

- 15 Step 2: Refer to Table 5-1, which indicates that, on average, FDS underpredicts target
 16 temperatures with a bias factor, δ , of 0.98. Calculate the *adjusted model prediction*:

$$\mu = \frac{M}{\delta} = \frac{280 \text{ °C}}{0.98} \cong 286 \text{ °C} \quad (5-7)$$

- 17 Referring again to Table 5-1, calculate the standard deviation of the distribution:

$$\sigma = \tilde{\sigma}_M\left(\frac{M}{\delta}\right) = 0.18\left(\frac{280 \text{ °C}}{0.98}\right) \cong 51 \text{ °C} \quad (5-8)$$

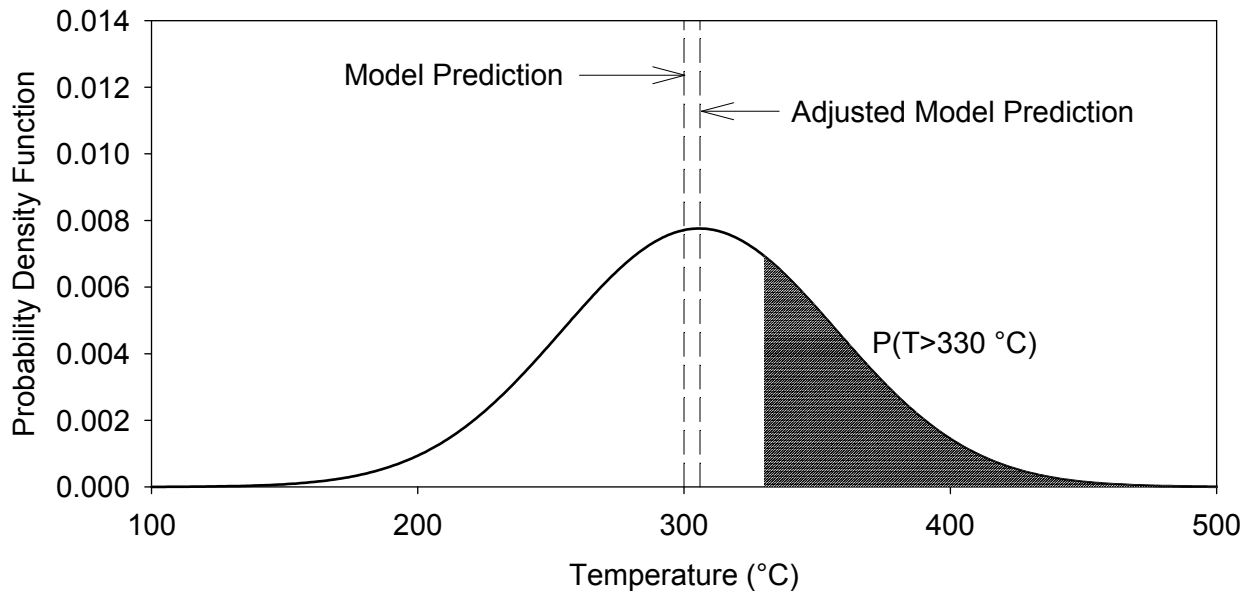
- 18 Step 3: Calculate the probability that the actual cable temperature would exceed 330°C (626°F):

$$P(T > 330 \text{ °C}) = \frac{1}{2} \operatorname{erfc}\left(\frac{T - T_0 - \mu}{\sigma\sqrt{2}}\right) = \frac{1}{2} \operatorname{erfc}\left(\frac{330 \text{ °C} - 20 \text{ °C} - 286 \text{ °C}}{51 \text{ °C} \sqrt{2}}\right) \cong 0.32 \quad (5-9)$$

⁷ Excel 2007 does not evaluate $\operatorname{erfc}(x)$ for negative values of x , even though the function is defined for all real x . In such cases, use the identity $\operatorname{erfc}(-x) = 2 - \operatorname{erfc}(x)$.

VALIDATION RESULTS

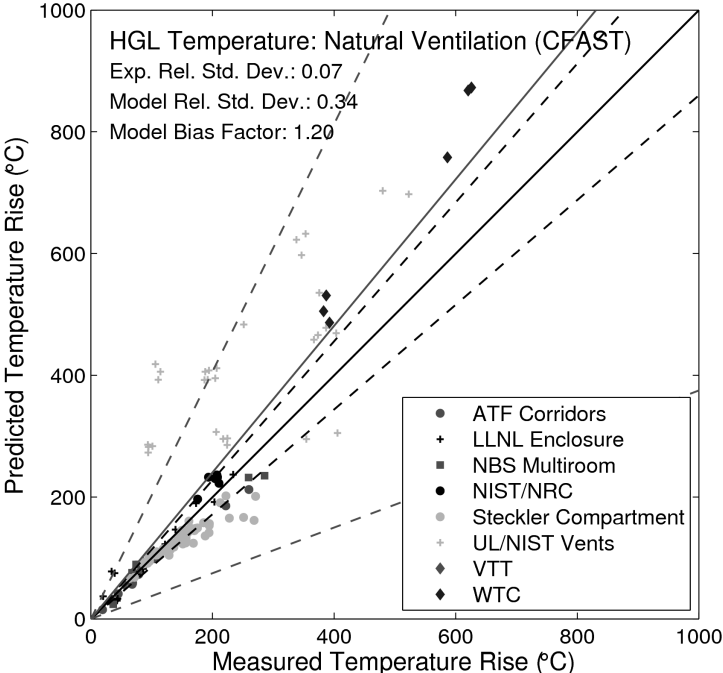
- 1 The process is shown graphically in Figure 5-2. The area under the “bell curve” for temperatures
- 2 higher than 330 °C (626 °F) represents the probability that the actual cable temperature would
- 3 exceed that value.



4
5 **Figure 5-2. Normal distribution of the “true” peak temperature of an electrical cable**

6 **5.1.2 Limitation of the Method**

7 The relatively simple method described above for quantifying model uncertainty is based on the
8 assumption that the relative difference between model prediction and experimental
9 measurement is normally distributed. For large data sets, this can be checked qualitatively by
10 visual inspection. For example, for the data shown in Figure 5-1, the quantity $\ln(M/E)$, when
11 presented in the form of a histogram, does appear to be normally distributed. However, in some
12 cases the data do not appear to be normally distributed. Consider, for example, the data shown
13 in Figure 5-3. The model uncertainty bounds (red dashed lines) do not appear to evenly straddle
14 the data. In this case, the data from one set of experiments (UL/NIST Vents) tend to skew the
15 distribution. It might be argued that this data be analyzed using a different assumption about the
16 distribution. However, this would seriously complicate the presentation of the results and make it
17 much more difficult to apply the uncertainty metrics in the way presented above.



1
2 **Figure 5-3. Example of data that are non-normally distributed.**
3

1 **5.2 Validation Results for Selected Output Quantities**

2 This section presents the results that summarize the accuracy of the models. For each quantity
3 of interest (e.g., oxygen concentration), the results of the empirical correlations, zone models,
4 and CFD model are discussed separately. While it is not possible to comment on each and
5 every point within the scatter plots, noticeable trends are discussed.

6 The intent is to compare the models to as much of the experimental data as possible. Because
7 it includes the most detailed physics, the CFD model (FDS) is compared against all of the data.
8 In some cases, the zone and empirical models cannot be applied to all of the data, in which
9 case the specific data or experiments that are excluded are described.

10 **5.2.1 HGL Temperature**

11 The HGL temperature, as discussed in Section 2.2, is particularly important in NPP fire
12 scenarios because it is an indicator of target damage away from the ignition source. For typical
13 electrical cable types (thermoplastic and thermoset), the damage criteria are 205 °C (400 °F)
14 and 330 °C (626 °F) respectively (see Table 8-2 in Volume 2 of NUREG/CR-6850
15 (EPRI 1011989)). The empirical correlations and zone models typically predict an average HGL
16 temperature, while CFD models predict the local gas temperature in each computational grid
17 cell. For the purpose of comparing all of the models with experimental measurements, both the
18 CFD predictions and experimental measurements of local gas temperatures can be spatially
19 averaged in the form of an HGL temperature.

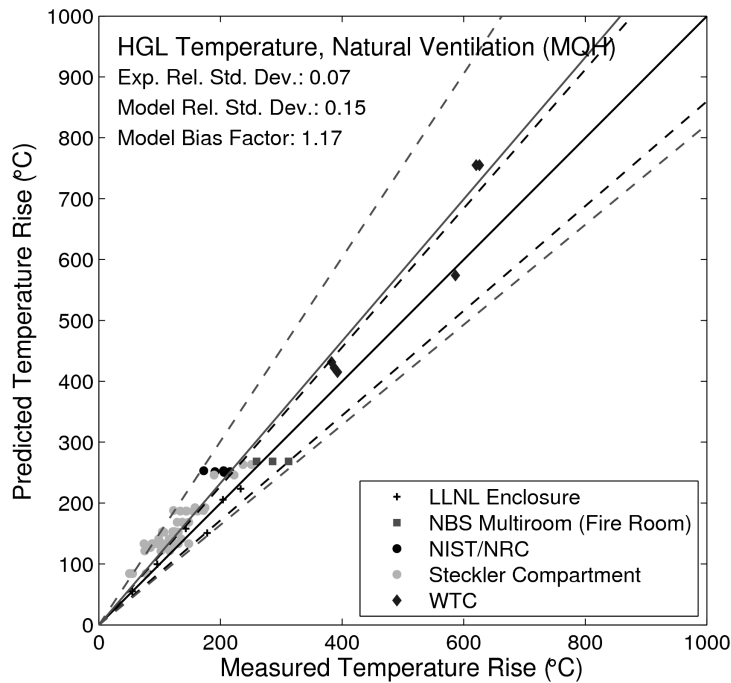
20 Because different empirical correlations govern compartments that are naturally ventilated,
21 mechanically ventilated, or unventilated, the results for HGL Temperature are divided into three
22 categories: natural, forced, and no ventilation.

23 **5.2.1.1 Natural Ventilation**

24 Natural ventilation refers to compartments with no HVAC system operational during the test and
25 openings to the outside. The peak measured temperature rise for the naturally ventilated
26 compartment experiments ranges from approximately 0 °C (32 °F) to 700 °C (1292 °F), with
27 most of the data lying at 400 °C (752 °F) or below. This latter temperature range is typical of
28 fires that can potentially damage equipment such as electrical cables.

29 Empirical Correlation: The results for the MQH correlation are shown in Figure 5-4. The
30 validation results from all of the experiments are within or above experimental uncertainty.
31 There is no indication of systematic underpredictions of HGL temperatures. Note that the
32 correlations only included a subset of the experimental data from the NBS Multiroom
33 Experiments (measurements located in the fire room) because the empirical correlation cannot
34 account for multiple rooms.

35 Note that the MQH correlation assumes that the ceiling, walls, and floor are composed of a
36 single material. Discussion is provided in Karlsson and Quintiere (2000) to calculate an effective
37 heat-transfer coefficient for compartments with different ceiling, wall, and floor materials as well
38 as materials composed of multiple layers in the MQH correlation. However, the discussion does
39 not provide details on calculating the thermal penetration time through these complex materials.
40 The validation results do not include those of the UL/NIST Vents Experiments (because of the
41 presence of ceiling vents), the ATF Corridors Experiments (because of their multi-story
42 compartment configuration), or the VTT Experiments (because of vents that were located high
43 in the compartment, complex wall lining materials, and irregular geometry).

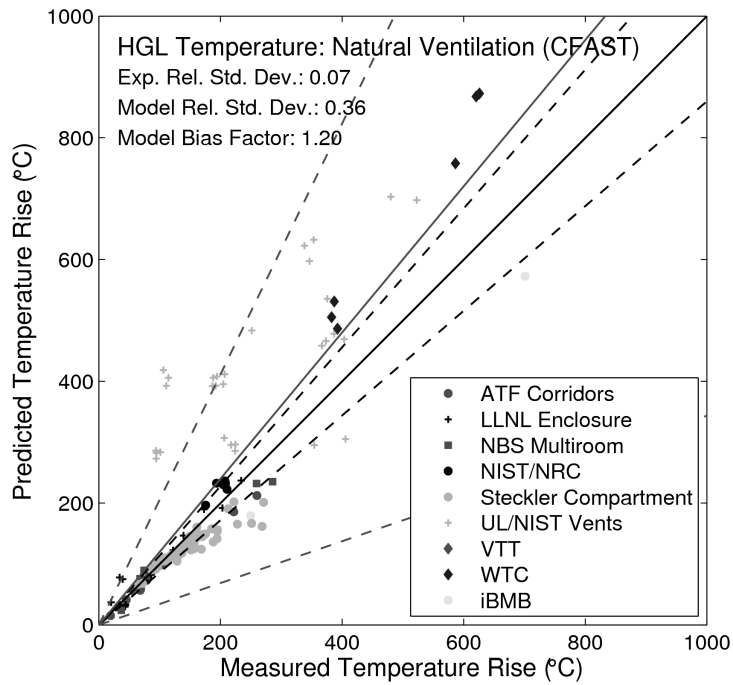


1

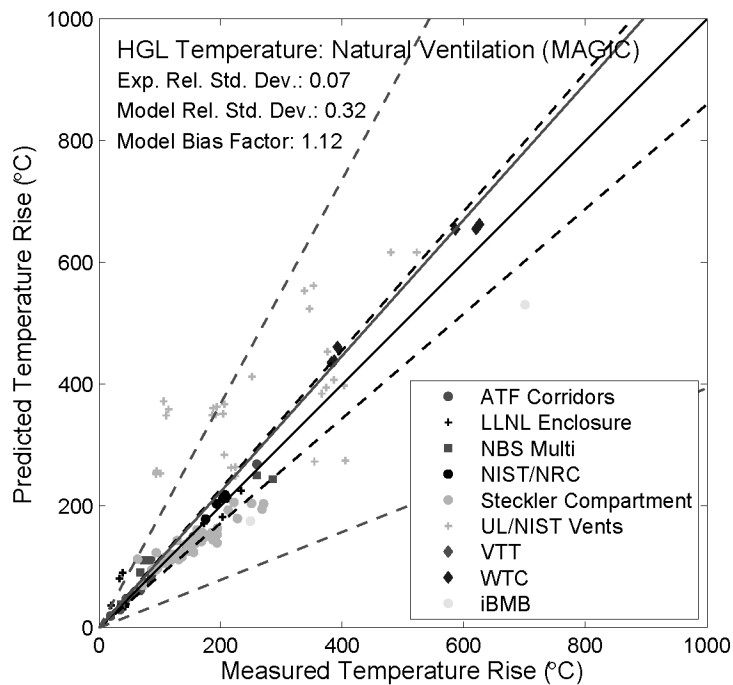
2 **Figure 5-4. HGL Temperature, Natural Ventilation (MQH).**

3 Zone Models: The results for CFAST and MAGIC are shown in Figure 5-5 and Figure 5-6
 4 respectively. Typically, the models slightly overpredict the HGL temperature, particularly for
 5 tests with a relatively large fire. This is likely caused by simplifying assumptions for zone models
 6 in calculating radiation to layers, to compartment surfaces, and through vents to the outside or
 7 other compartments. The UL/NIST Vents experiments are noticeably overpredicted. These tests
 8 include large vents in the ceiling of the compartment that might extend beyond the original vent
 9 sizes of the empirical correlation used to determine flow through ceiling vents. In addition, the
 10 combination of larger HGL temperature and smaller HGL depth compared to the experimental
 11 data suggest that part of the difference may be attributed to the reduction method used to
 12 estimate layer temperature and position from the individual temperature measurements in the
 13 experiments.

VALIDATION RESULTS

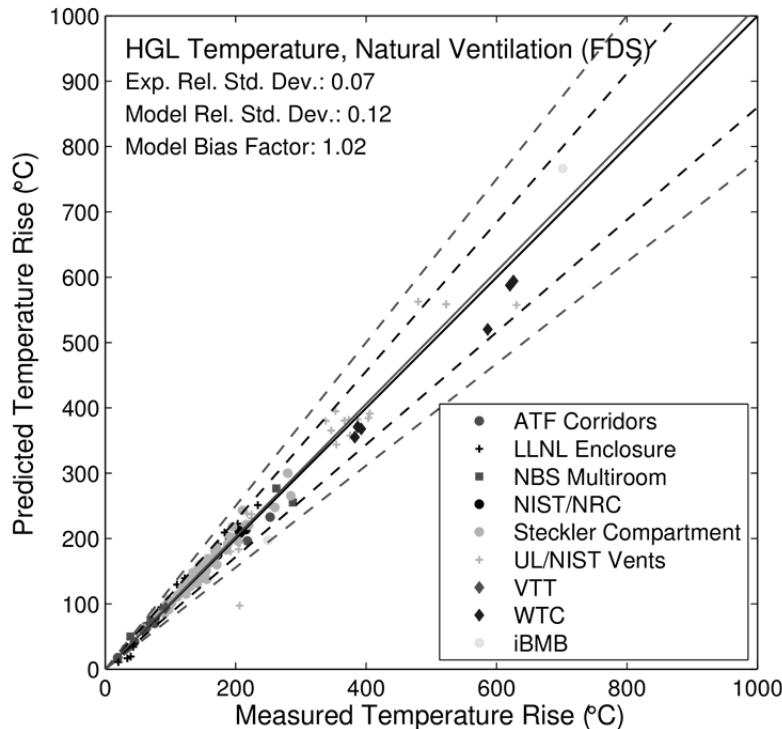


1
2 **Figure 5-5. HGL Temperature, Natural Ventilation (CFAST).**



3
4 **Figure 5-6. HGL Temperature, Natural Ventilation (MAGIC).**

1 CFD Model: The FDS results are shown in Figure 5-7. There is no obvious bias in the model
 2 predictions and there are no particular trends in the data. The relatively low bias and model
 3 relative standard deviation suggest that FDS HGL predictions are close to experimental
 4 uncertainty. FDS does not calculate an HGL temperature directly. Rather, it predicts the gas
 5 temperatures at the same locations as the experimental measurements, and the HGL
 6 temperature is calculated in the exact same way as it is for the experimental data.



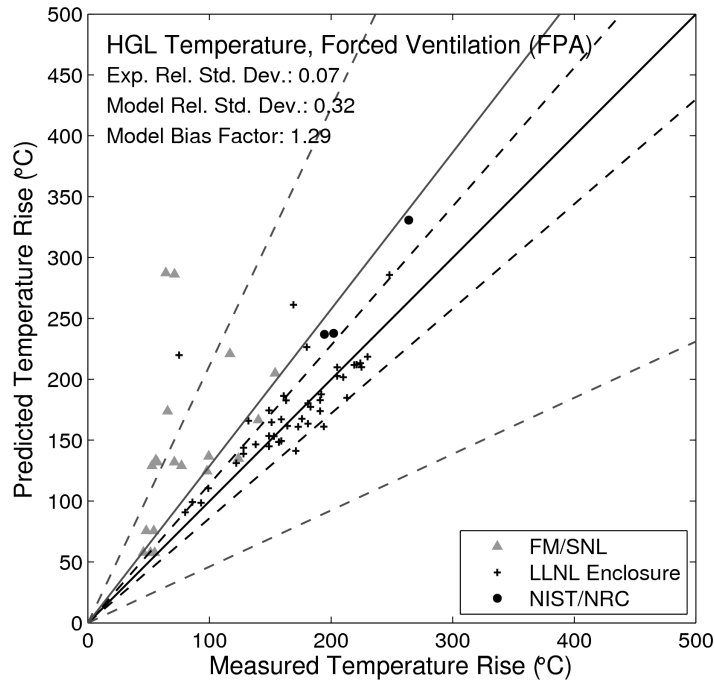
7
 8 **Figure 5-7. HGL Temperature, Natural Ventilation (FDS).**

9 **5.2.1.2 Forced Ventilation**

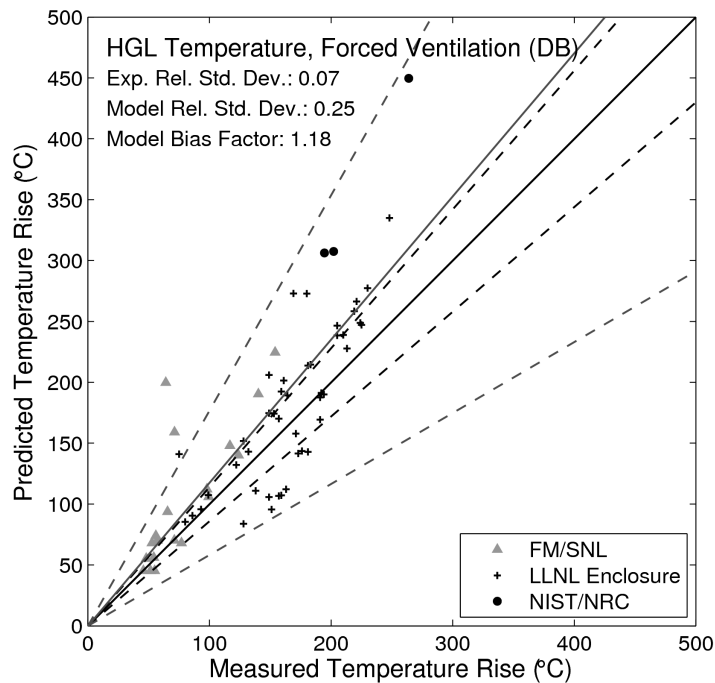
10 The peak measured temperature rise for the forced-ventilation compartment experiments
 11 ranges from approximately 0 °C (32 °F) to 300 °C (572 °F).

12 Empirical Correlation: The results for the FPA and DB correlations are shown in Figure 5-8 and
 13 Figure 5-9 respectively. On average, the FPA correlation tends to predict a higher HGL
 14 temperature than the DB correlation, which is reflected in the larger model bias factor for the
 15 FPA correlation. Note that the predictions for the LLNL Enclosure Experiments are in better
 16 agreement with the FPA correlation because they were used to develop the FPA correlation.
 17 The validation results do not include the VTT Experiments (because of those experiments'
 18 complex wall-lining materials and irregular geometry, as discussed in Section 5.2.1.1).

VALIDATION RESULTS



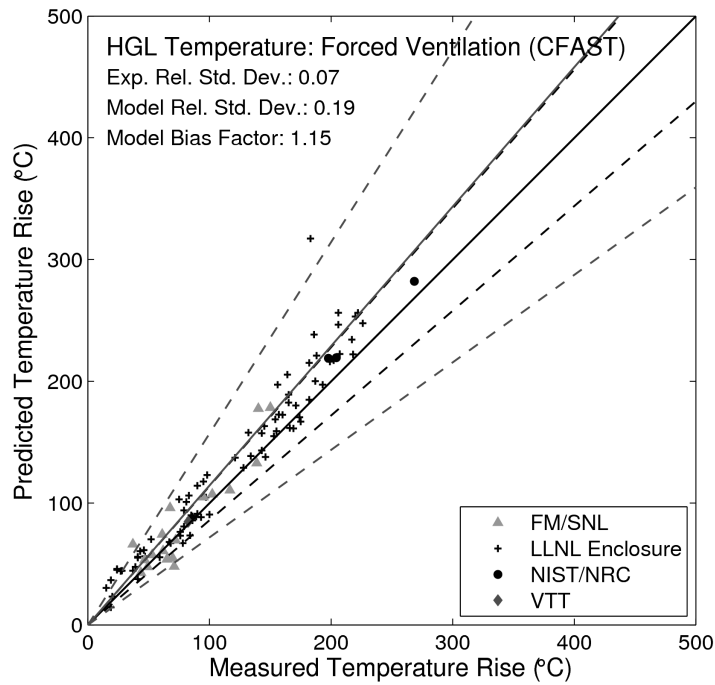
1
2 **Figure 5-8. HGL Temperature, Forced Ventilation (FPA).**



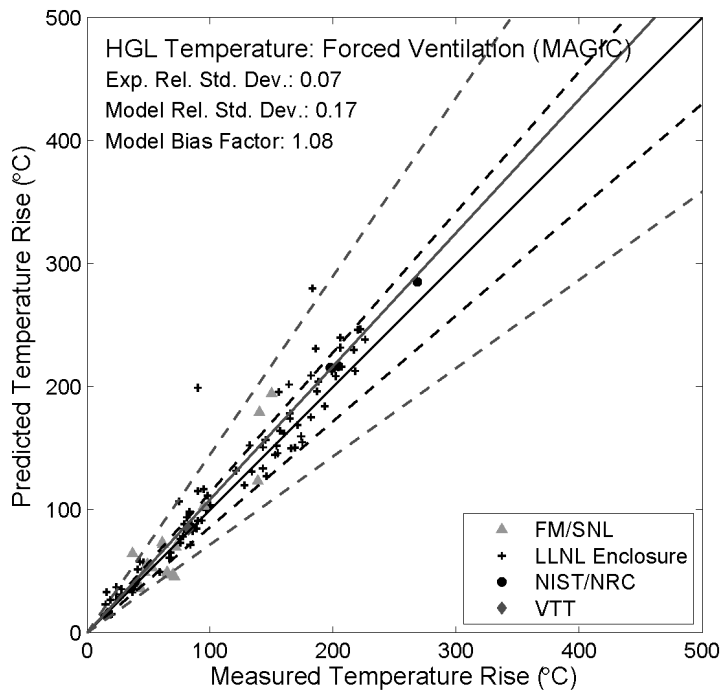
3
4 **Figure 5-9. HGL Temperature, Forced Ventilation (DB).**

- 1 Zone Models: The results for CFAST and MAGIC are shown in Figure 5-10 and Figure 5-11
- 2 respectively. Typically, the models overpredict the HGL temperature in forced-ventilation tests.
- 3 The overprediction is likely caused by the simplified mixing assumption applied to the
- 4 forced-ventilation air that is injected into the upper and lower layer.

VALIDATION RESULTS

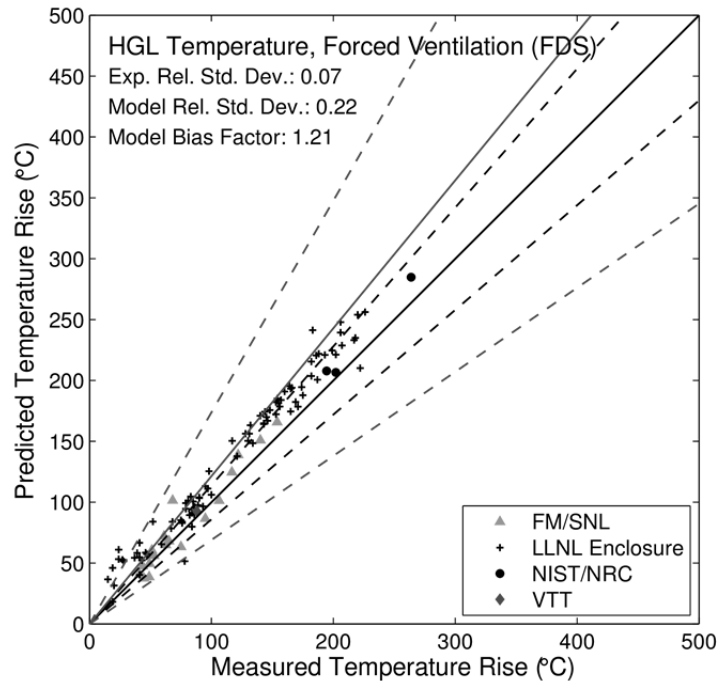


1
2 **Figure 5-10. HGL Temperature, Forced Ventilation (CFAST).**



3
4 **Figure 5-11. HGL Temperature, Forced Ventilation (MAGIC).**

1 CFD Model: The FDS results are shown in Figure 5-12. The FDS results are dominated by the
 2 LLNL Enclosure Experiments, which had the largest number of tests. For this data set, the
 3 greatest inaccuracies occur for relatively low temperatures on which the effects of the forced
 4 ventilation are most pronounced. For higher temperatures, the predictions are more accurate
 5 than is implied by the computed model uncertainty.



6
 7 **Figure 5-12. HGL Temperature, Forced Ventilation (FDS).**

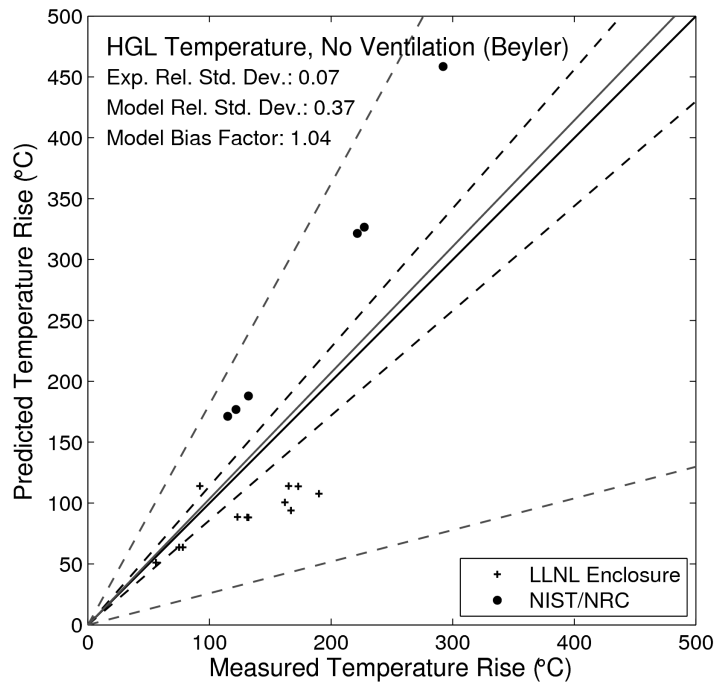
8 **5.2.1.3 No Ventilation**

9 Compartments with no ventilation are typically closed with only leakage paths connecting
 10 neighboring compartments or the outside. The peak measured temperature rise for the
 11 unventilated compartment experiments ranges from approximately 0 °C (32 °F) to 300 °C
 12 (572 °F).

13 Empirical Correlation

14 The results for the Beyler correlation are shown in Figure 5-13. The validation results are
 15 characterized by a limited set of experiments. The model bias factor might not be an indication
 16 of the expected results for a given scenario, and the large model relative standard deviation
 17 accounts for the uncertainty associated with the model. The model bias factor is a result of
 18 under- and overpredictions from two sets of experiments with very different compartment
 19 geometries, which might be the reason for the difference in the results for the two data sets. The
 20 validation results do not include those for the NBS Multiroom Experiments (because of the
 21 presence of multiple compartments).

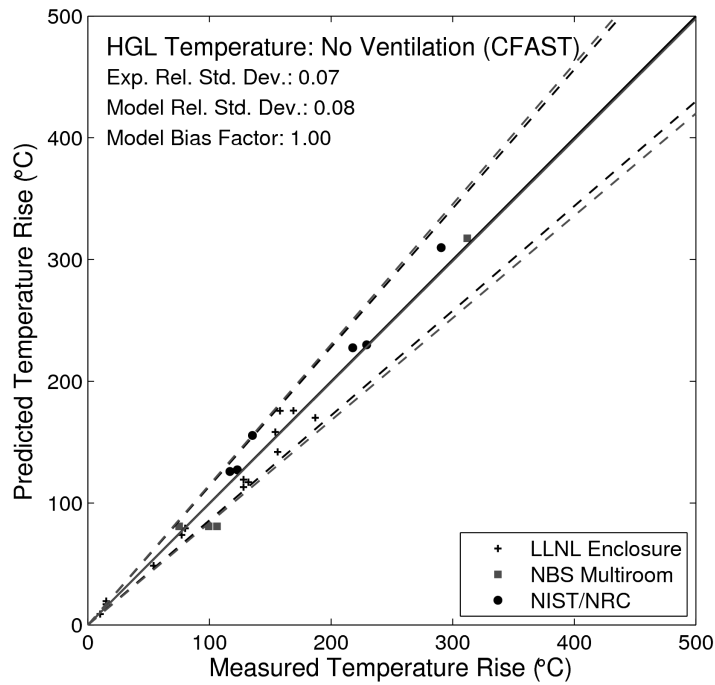
VALIDATION RESULTS



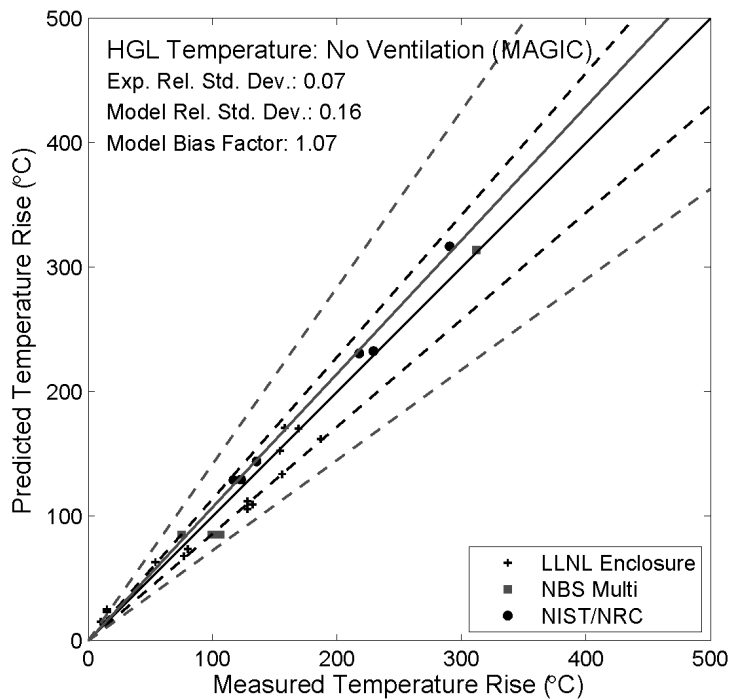
1

2 **Figure 5-13. HGL Temperature, No Ventilation (Beyler).**

3 Zone Models: The results for CFAST and MAGIC are shown in Figure 5-14 and Figure 5-15
4 respectively. CFAST predictions of HGL temperature in closed compartments are nearly within
5 experimental uncertainty and reflect the simpler scenarios without vent flows. MAGIC results are
6 comparable to those from CFAST.



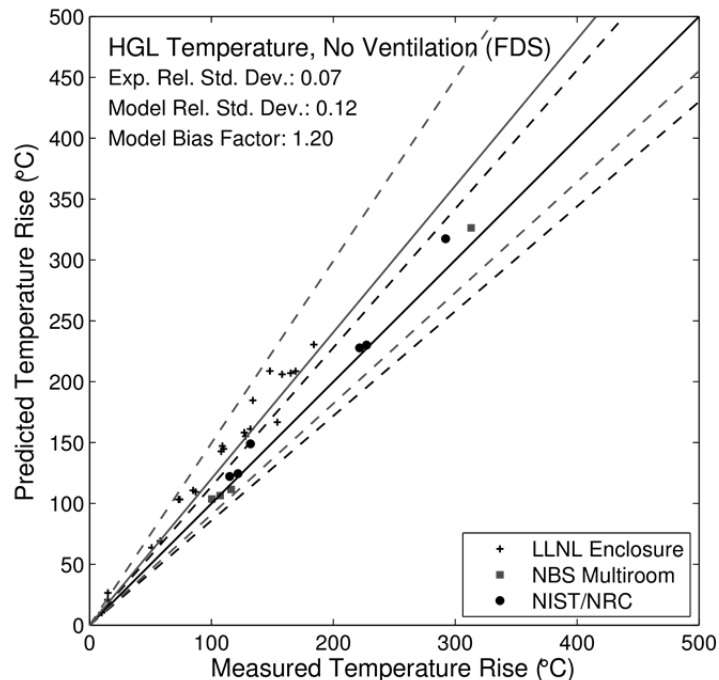
1
 2 **Figure 5-14. HGL Temperature, No Ventilation (CFAST).**



3
 4 **Figure 5-15. HGL Temperature, No Ventilation (MAGIC).**

VALIDATION RESULTS

1 CFD Model: The FDS results are shown in Figure 5-16. The FDS results are most heavily
2 influenced by the LLNL Enclosure Experiments. The NBS and NIST/NRC results do not indicate
3 a particular bias. In the LLNL tests, the experiments were cut short because of the danger
4 posed by a lack of oxygen in a fuel-rich compartment. The temperatures did not reach a steady
5 state before the experiments were ended. The FDS predictions are less accurate during the
6 early stage of the experiments because not enough information was given about the ramp-up of
7 the fuel flow rate.



8

9 **Figure 5-16. HGL Temperature, No Ventilation (FDS).**

10 **5.2.2 HGL Depth**

11 The depth of the HGL is also important in NPP fire scenarios because it indicates whether a
12 given target is immersed in high-temperature gases. HGL depth is a direct output of a two-zone
13 model, and it can be calculated from local gas temperatures predicted by a CFD model. The
14 empirical correlations can predict the HGL depth only for very simple closed-compartment
15 geometries.

16 The range of HGL depth is approximately 1 m (3.3 ft) to 4 m (13.1 ft) with the exception of the
17 VTT experiments, which were conducted in a 19 m (62.3 ft) tall test building.

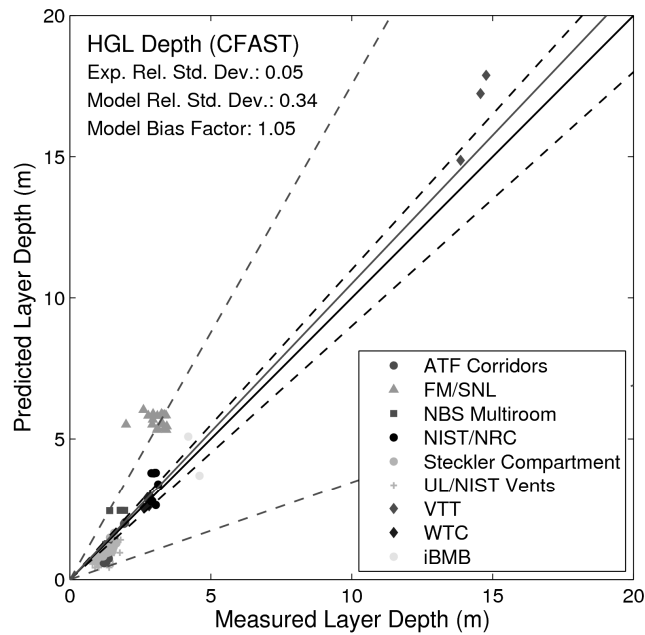
18 Zone Models: The results for CFAST and MAGIC are shown in Figure 5-17 and Figure 5-18
19 respectively. HGL depth is slightly overpredicted by the zone models. Of particular note are the
20 FM/SNL tests, which are closed-compartment experiments with and without forced ventilation.
21 For closed-door tests, visual observations typically show that the HGL fills the entire

22

VALIDATION RESULTS

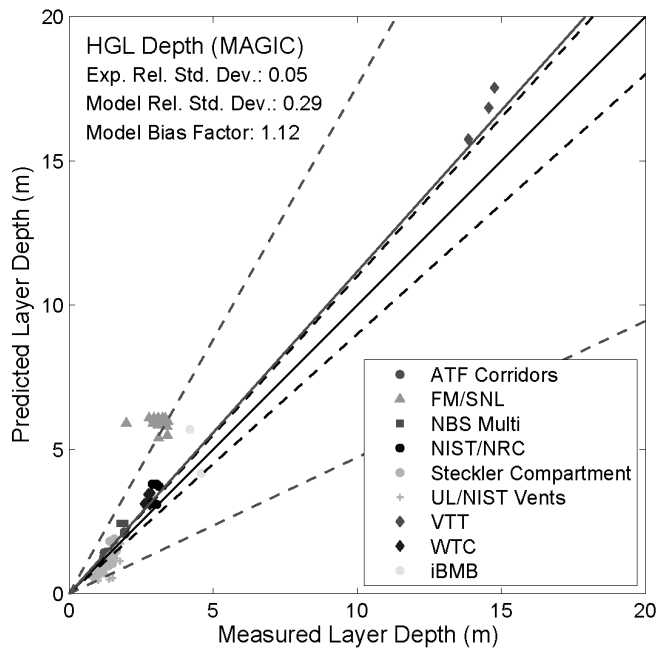
- 1 compartment volume from floor to ceiling, which is inconsistent with the calculated results for
- 2 the experimental data. Thus, the calculated experimental values of HGL height for closed-door
- 3 tests might not be as meaningful as the open-compartment tests for comparison to model
- 4 results.

VALIDATION RESULTS



1

2 **Figure 5-17. HGL Depth (CFAST).**

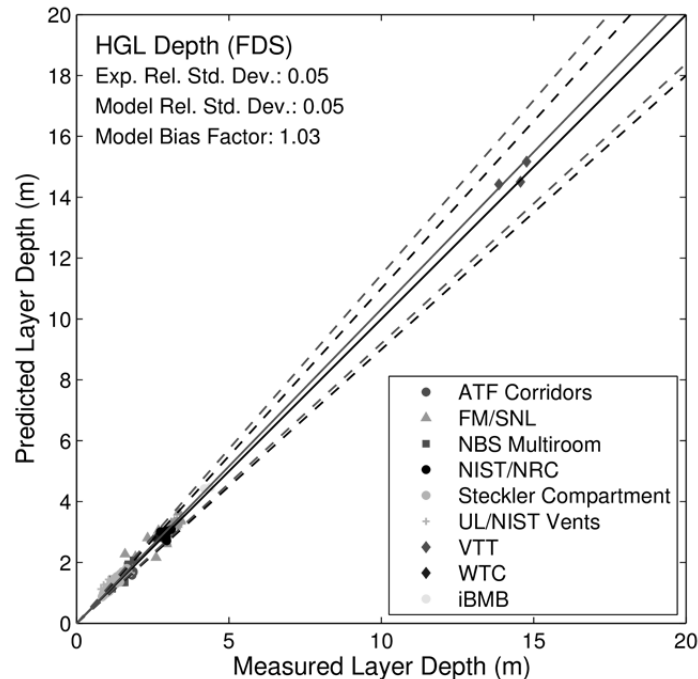


3

4 **Figure 5-18. HGL Depth (MAGIC).**

5 CFD Model: The FDS results are shown in Figure 5-19. The FDS results are nearly within
6 experimental uncertainty. The reason for this is that the HGL depth is derived from the FDS

1 temperature predictions in the exact same way as the experimental measurements. Thus,
 2 reasonable agreement in the vertical temperature profile leads to a very close match in HGL
 3 depth. This is not true of the zone models and empirical correlations; their definitions of HGL
 4 depth are not the same as that of the experiments.



5
 6 **Figure 5-19. HGL Depth (FDS).**

7 **5.2.3 Ceiling Jet Temperature**

8 The ceiling jet is the shallow layer of hot gases below the ceiling that spreads radially from the
 9 centerline of the fire plume. The ceiling jet has a higher temperature than the overall
 10 temperature of the HGL, and therefore it is important in NPP fire scenarios in which targets are
 11 located just below the ceiling. A variety of empirical correlations that predict the ceiling jet
 12 temperature are embedded in the zone models. CFD models compute the ceiling jet
 13 temperature directly from the fundamental equations of fluid motion.

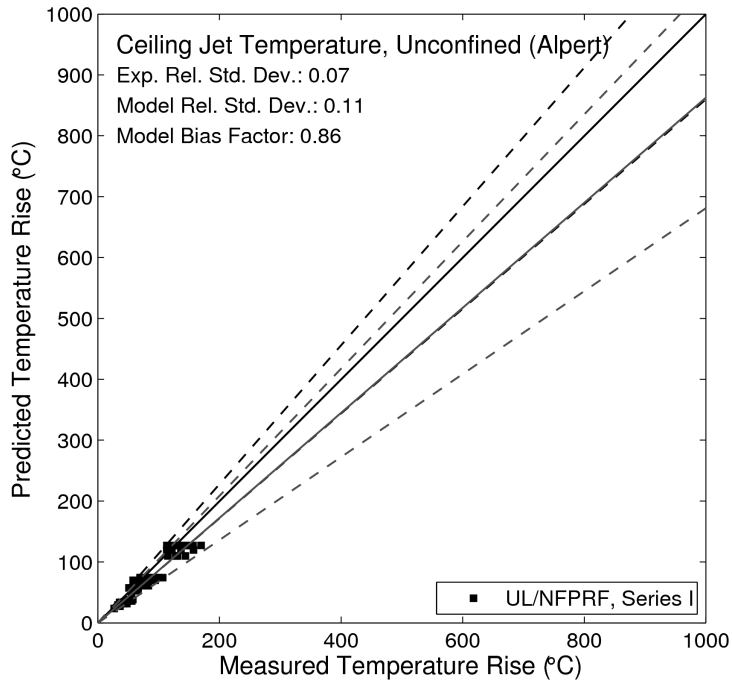
14 The ceiling-jet temperature measurements range from 0 °C (32 °F) to 900 °C (1652 °F). This
 15 upper value is typical of a flashed-over compartment or a compartment in which flames impinge
 16 on the ceiling.

17 Empirical Correlations: Alpert’s correlation of ceiling jet temperature was developed for
 18 unconfined ceilings against which a hot gas layer is not expected to form. However, it is often
 19 applied in compartment fire scenarios in which an HGL does form. The use of the ceiling jet
 20 correlation in a compartment with the presence of an HGL can result in an underprediction of
 21 the measured ceiling jet temperature by approximately 70 percent. To call attention to this fact,
 22 the scatter plots divide the relevant experiments into two categories: Figure 5-20 in which the
 23 ceiling is unconfined and Figure 5-21 in which the ceiling is confined and an HGL develops
 24 within a compartment.

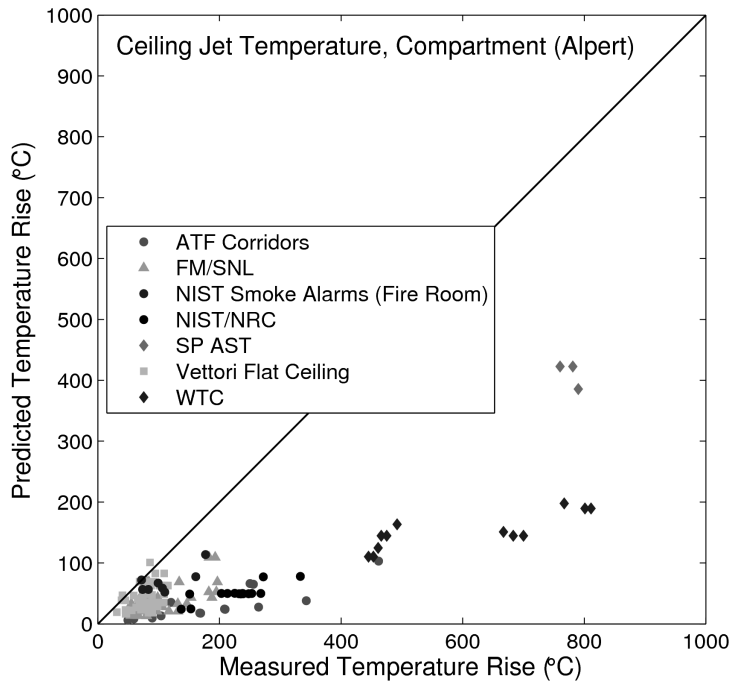
VALIDATION RESULTS

1 Figure 5-21 illustrates the underprediction that occurs when the HGL is not accounted for in the
2 ceiling jet temperature calculations. The fact that ceiling jet correlations like Alpert's do not
3 account for the influence of the HGL has been noted by the developers of zone models such as
4 CFAST and MAGIC, which use a modified plume algorithm (Evans, 1985; Cooper, 1988) to
5 account for the entrainment of HGL gases in the upper portion of the plume. Simply adding the
6 ceiling jet temperature rise predicted by the correlation and the predicted HGL temperature rise
7 together to estimate the true ceiling jet temperature has been suggested as an engineering
8 approximation to the results of the more complicated modified plume algorithms (Mowrer, 1992).
9 This strategy was used for the FIVE-Rev1 ceiling jet calculations in the 2007 edition of
10 NUREG-1824 (EPRI 1011999).

11 The quantification of Table 3-1 from the 2007 edition of NUREG-1824 (EPRI 1011999) that is
12 presented as Table 4-1 in NUREG-1934 (EPRI 1023259) shows a bias factor for the FIVE-Rev1
13 ceiling jet temperature rise of 1.84. This value indicates that FIVE-Rev1 would overpredict the
14 ceiling jet temperature rise by more than 80 percent as a result of the simplification. For the
15 empirical correlations, this supplement focuses solely on the prediction of ceiling jet temperature
16 rise in an unconfined environment. The prediction of sprinkler or detector activation and ignition
17 of cables exposed to a ceiling jet in a compartment with an HGL are important components of a
18 fire-hazard analysis. Future work will be undertaken to develop empirical correlations that
19 implement appropriate modified plume or other algorithms to calculate ceiling jet temperature
20 rise in a confined environment.



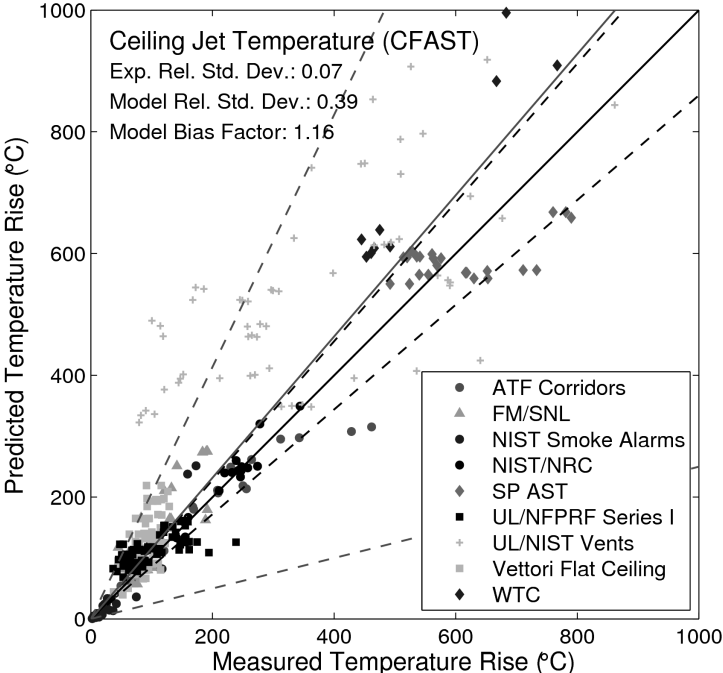
1
 2 **Figure 5-20. Ceiling Jet Temperature, Unconfined Ceiling (Alpert).**



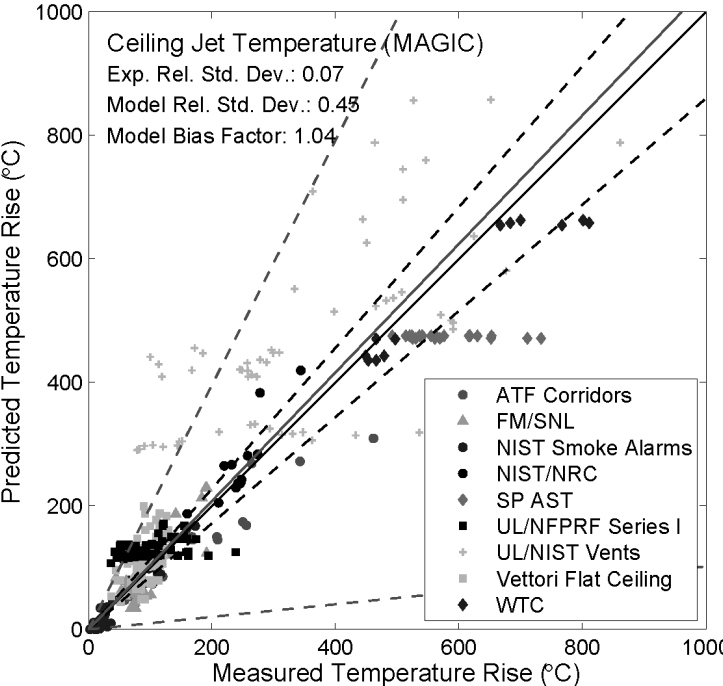
3
 4 **Figure 5-21. Ceiling Jet Temperature, Ceiling of a Confined Compartment (Alpert).**

VALIDATION RESULTS

1 Zone Models: The results for CFAST and MAGIC are shown in Figure 5-22 and Figure 5-23
2 respectively. Both CFAST and MAGIC predict similar results for ceiling jet temperatures less
3 than about 400 °C (752 °F). At higher temperatures, CFAST predicts higher temperatures than
4 MAGIC. Both models include algorithms to account for the presence of higher gas temperatures
5 near the ceiling surfaces in compartments involved in a fire. The ceiling jet algorithm predicts
6 gas temperature and velocity under a flat, unconstrained ceiling. Limitations of the algorithm can
7 been seen in the predictions for the SP, AST, and WTC tests where the zone mode
8 approximations cluster model predictions together compared to the wider range of experimental
9 measurements. As with the HGL temperature, an overprediction in temperature for the UL/NIST
10 Vents series is seen with the ceiling jet temperature. Because ceiling jet temperatures are
11 calculated as a rise above HGL temperature, this is consistent.



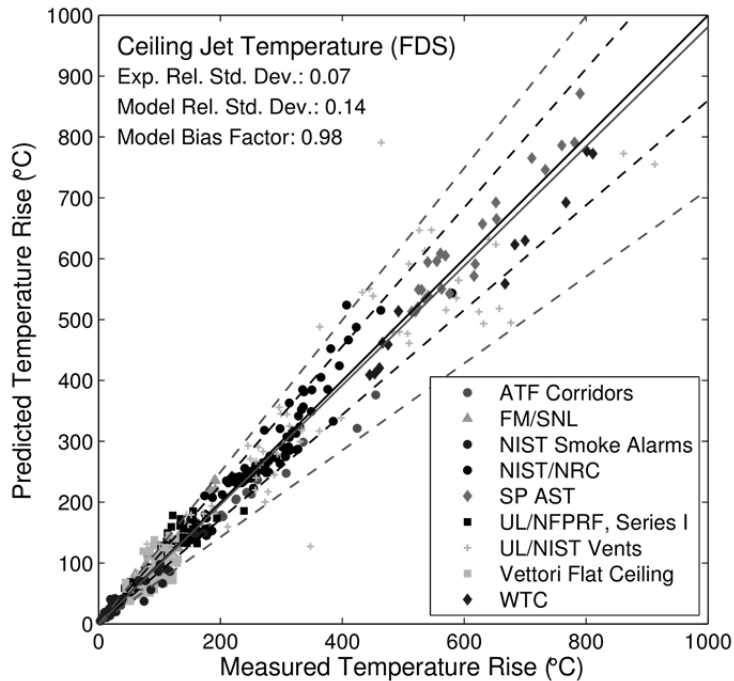
1
2 **Figure 5-22. Ceiling Jet Temperature (CFAST).**



3
4 **Figure 5-23. Ceiling Jet Temperature (MAGIC).**

VALIDATION RESULTS

- 1 CFD Model: The FDS results are shown in Figure 5-24. FDS does not have a specific ceiling jet
2 model; it calculates temperatures near the ceiling based on the overall solution of the governing
3 equations. The FDS results do not indicate any particular bias or trend. The model uncertainty is
4 primarily determined by the low-temperature data for which the inaccuracies are expected to be
5 relatively higher because random initial conditions and background motion play more of a role.



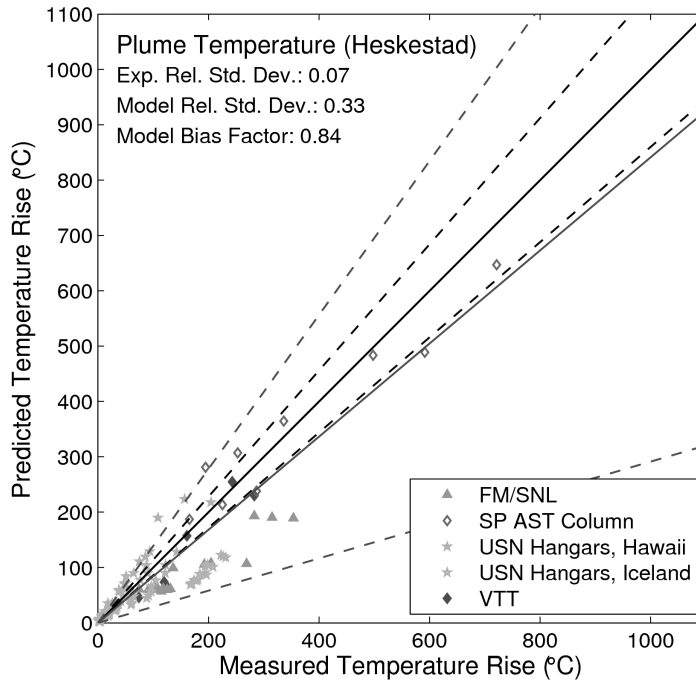
6
7 **Figure 5-24. Ceiling Jet Temperature (FDS).**

8 **5.2.4 Plume Temperature**

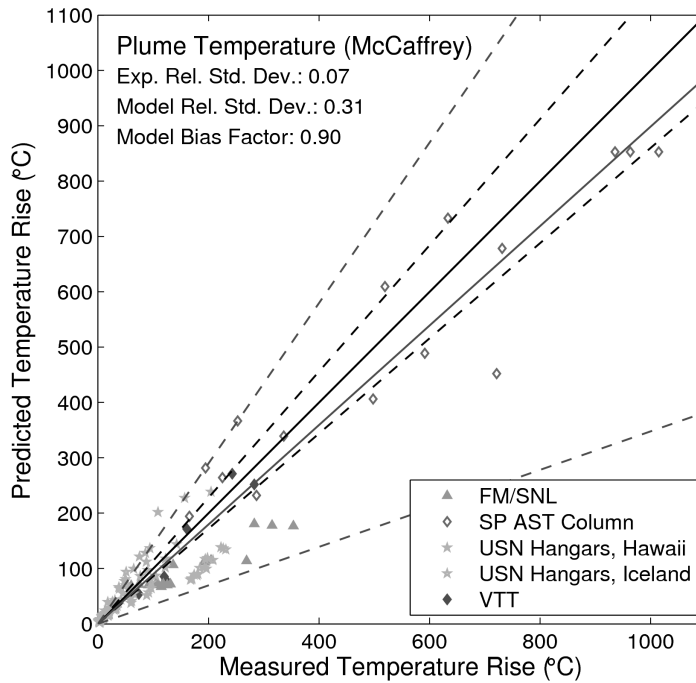
9 The fire plume transports hot gases into the HGL. Its temperature is greater than the ceiling-jet
10 and HGL temperature. It is particularly important in NPP fires because of the numerous
11 postulated scenarios that involve targets directly above a potential fire. A variety of empirical
12 correlations that predict the plume temperature are embedded in the zone models. CFD models
13 compute the plume temperature directly from the fundamental equations of motion.

14 The range of plume temperatures extends nearly to 1000 °C (1832 °F), which is within the flame
15 envelope. This is important when modeling fully immersed targets.

16 Empirical Correlations: The results for the Heskestad and McCaffrey correlations are shown in
17 Figure 5-25 and Figure 5-26 respectively. Note that the McCaffrey plume temperature
18 correlation includes results at higher temperatures than the Heskestad plume temperature
19 correlation because the Heskestad correlation is only valid above the mean flame height. These
20 correlations do not account for the thermal effects of the hot gas layer.



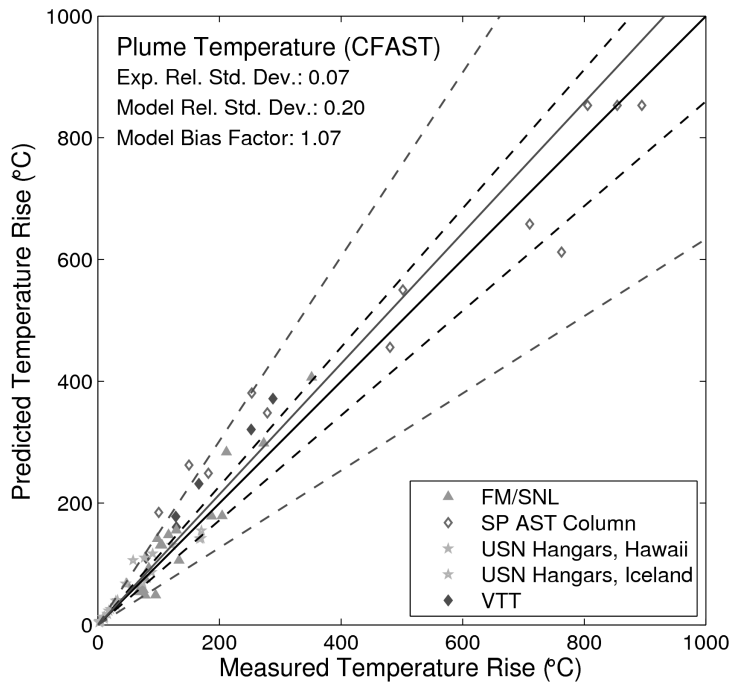
1
 2 **Figure 5-25. Plume Temperature (Heskestad).**



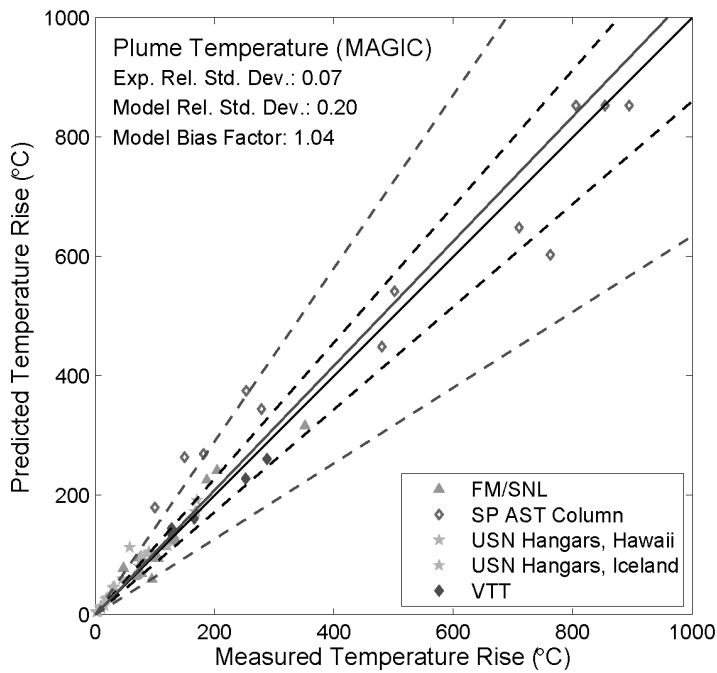
3
 4 **Figure 5-26. Plume Temperature (McCaffrey).**

VALIDATION RESULTS

- 1 Zone Models: The CFAST and MAGIC results for plume temperature are shown in Figure 5-27
- 2 and Figure 5-28 respectively. The zone models have a specific plume sub-model similar to the
- 3 sub-model they have for ceiling jets. Both models employ the McCaffrey plume correlation
- 4 supplemented by the HGL temperature. Similar to the cases for HGL and ceiling jet
- 5 temperature, a slight overprediction of the plume temperature is typical because the plume and
- 6 HGL temperatures are not purely additive.



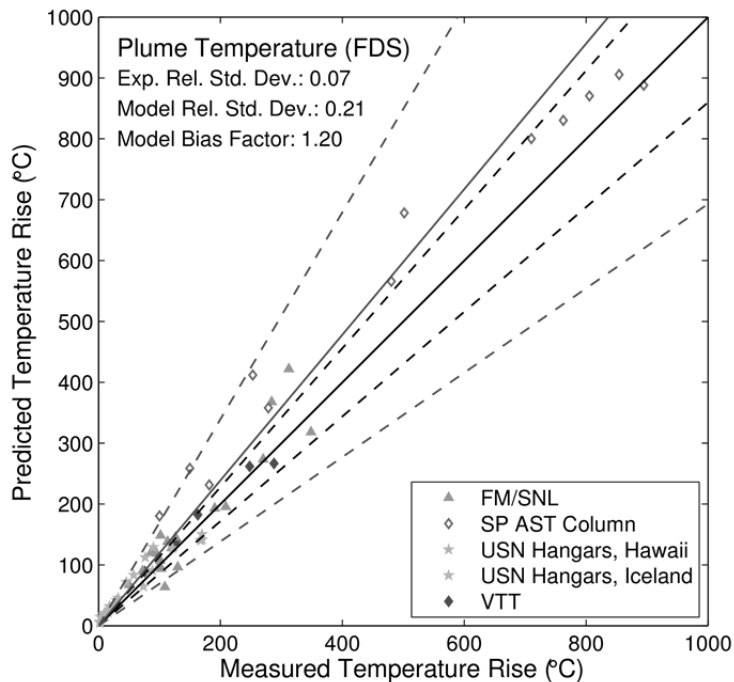
1
 2 **Figure 5-27. Plume Temperature (CFAST).**



3
 4 **Figure 5-28. Plume Temperature (MAGIC).**

VALIDATION RESULTS

1 **CFD Model:** The FDS results are shown in Figure 5-29. The uncertainty in the FDS predictions
2 results largely from the USN Hangar experiments in which relatively small fires were lit within
3 very large and drafty aircraft hangars. The HGL temperatures in these experiments were only a
4 few tens of degrees above ambient, and there was a substantial temperature stratification in the
5 hangars which was not included in the model. At the other end of the temperature scale, the SP
6 AST Column predictions are for a fully engulfing hydrocarbon pool fire. Because a single relative
7 uncertainty is applied to the model, the inaccuracy of the USN Hangar results is applied to the
8 entire set of data.



9
10 **Figure 5-29. Plume Temperature (FDS).**

11 **5.2.5 Oxygen Concentration**

12 Oxygen concentration is an indicator of a fire becoming underventilated, which is a precursor to
13 flashover. The zone models calculate the oxygen concentration in the upper and lower layers
14 and CFD models calculate the oxygen concentration in each grid cell. The empirical correlations
15 assessed in this study do not address oxygen concentration.

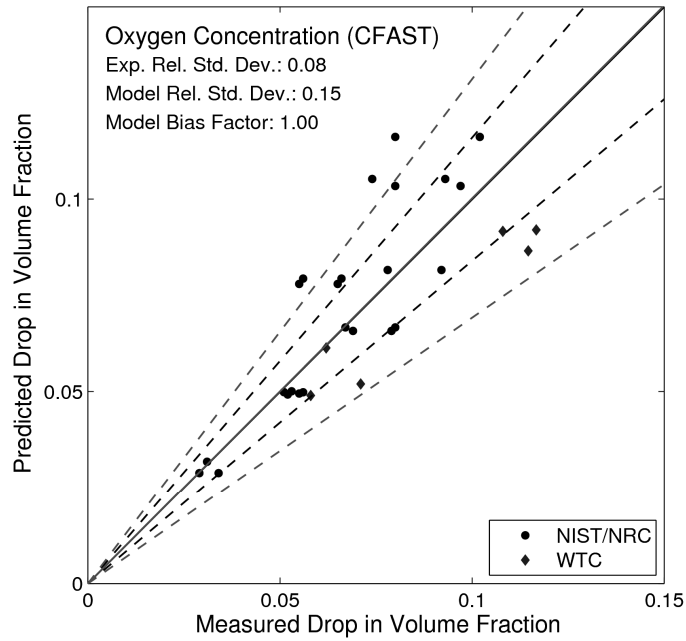
16 The measured decrease in oxygen ranges from approximately 3 percent to 12 percent.
17 A decrease in oxygen of approximately 6 percent indicates the start of oxygen-limited fire
18 conditions.

19

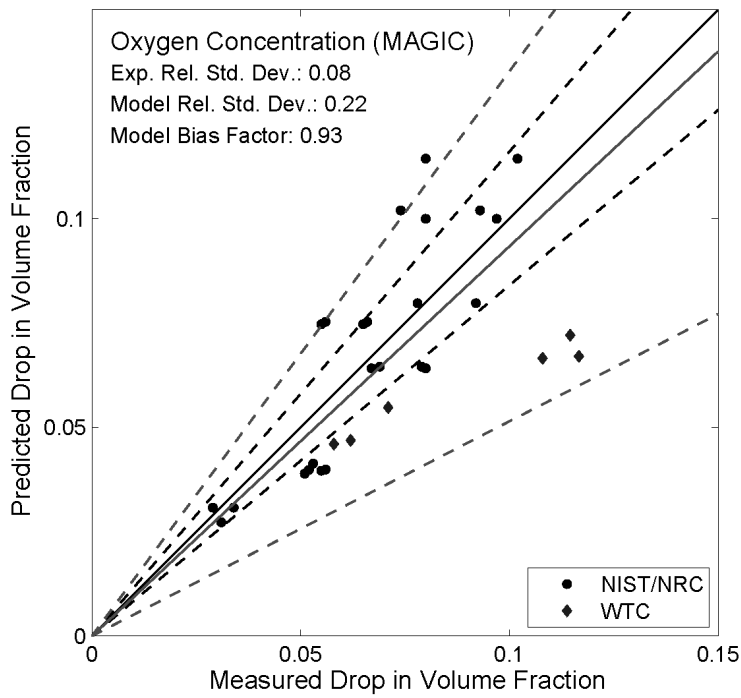
1

2 Zone Models: The results for CFAST and MAGIC are shown in Figure 5-30 and Figure 5-31
3 respectively. Species production in CFAST and MAGIC is based on user-defined product yields,
4 and both the burning rate and the resulting energy and species generation might be limited by
5 the oxygen available for combustion. When sufficient oxygen is available for combustion, the
6 heat-release rate for a constrained fire is the same as for an unconstrained fire. Mass and
7 species concentrations are tracked by the models as gases flow through openings in a structure
8 to other compartments in the structure or to the outdoors.

VALIDATION RESULTS



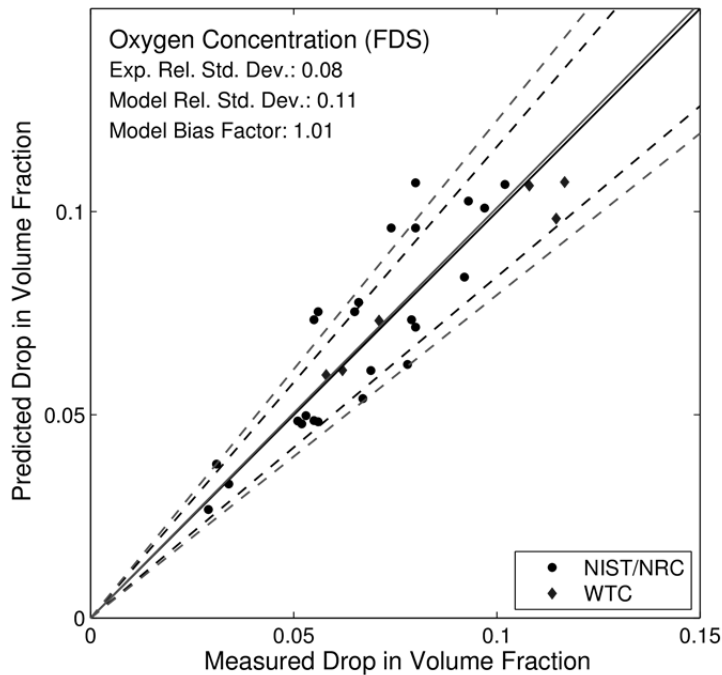
1
2 **Figure 5-30. Oxygen Concentration (CFAST).**



3
4 **Figure 5-31. Oxygen Concentration (MAGIC).**

1 For most tests, the models show similar results, with MAGIC trending to somewhat higher
 2 oxygen concentrations (lower predicted drop in volume fraction), particularly for very large fires
 3 (the WTC tests had peak HRR values of up to 3.5 MW). This is likely caused by different
 4 calculations for plume entrainment, vent flow mixing, and gas radiation in the two models,
 5 leading to additional entrainment by MAGIC and thus somewhat higher oxygen concentrations,
 6 lower layer temperatures, and lower heat fluxes to surrounding surfaces.

7 **CFD Model:** The FDS results are shown in Figure 5-32. The FDS results do not indicate any
 8 particular trend or bias. For both the NIST/NRC and WTC experiments, the fuel was n-heptane,
 9 which is predominantly composed of C_7H_{16} . The consumption rate of oxygen is proportional to
 10 the burning rate of the fuel, which is specified in the model. Thus, the consumption rate of
 11 oxygen is of comparable accuracy to the burning rate of the fuel. Although not shown here, the
 12 accuracy of the prediction of CO_2 is comparable to that of the prediction of O_2 because the basic
 13 fuel stoichiometry is known. However, the production rates of products of incomplete
 14 combustion, such as CO and soot, are not easily predicted; their predicted concentrations are
 15 less accurate.



16
 17 **Figure 5-32. Oxygen Concentration (FDS).**

18 **5.2.6 Smoke Concentration**

19 Smoke concentration is an important quantity for fire scenarios in areas where operators need
 20 to perform certain tasks. Zone and CFD models calculate smoke concentration by calculating
 21 the transport of soot from the fire throughout the compartment. Typically the soot yield is a
 22 specified model input. Note that the zone models evaluated here assume that soot behaves like
 23 the other product gases in that it does not deposit on compartment surfaces. In reality, soot can
 24 deposit on surfaces as a result of various deposition mechanisms, which reduces the gas-phase
 25 smoke concentration. Soot particles can also agglomerate to form larger particle sizes, which

VALIDATION RESULTS

1 can increase the soot-deposition rate. The CFD model evaluated here does account for some
2 soot-deposition mechanisms, but does not currently account for soot agglomeration. For these
3 reasons, the models tend to overestimate the smoke concentration (Hamins et al., 2006;
4 Gottuk et al., 2008).

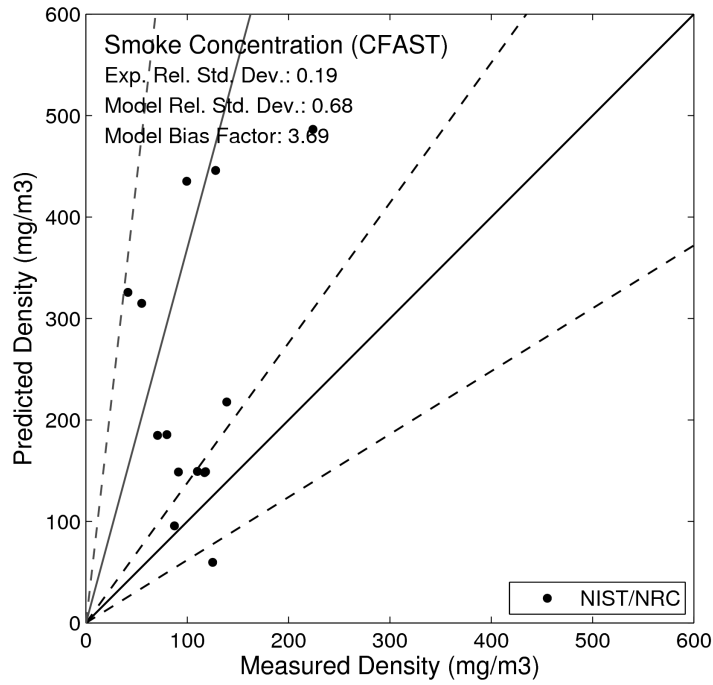
5 The measured smoke concentrations range from approximately 50 mg/m³ to 200 mg/m³. These
6 conditions are typical of sooty fires expected in industrial settings.

7 The empirical correlation spreadsheets do not contain smoke or visibility estimates.

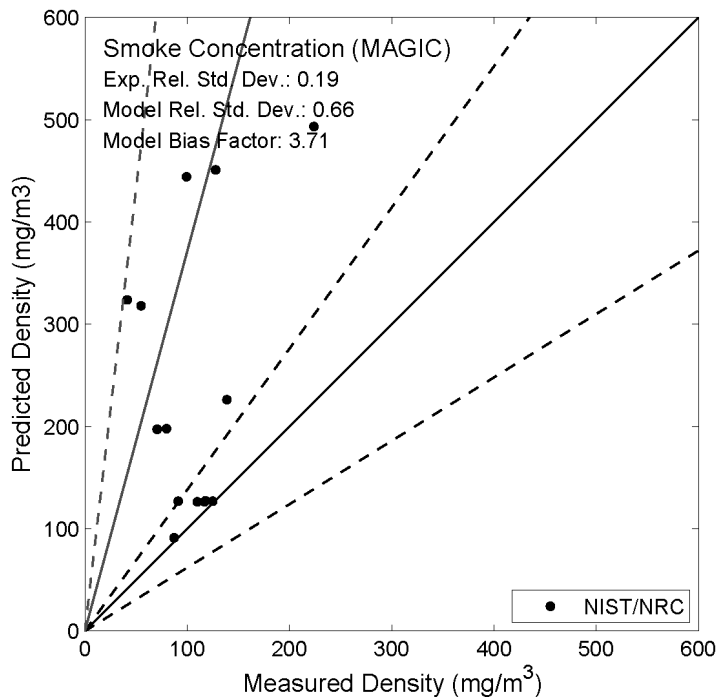
8 Zone Models: Zone models treat smoke like other combustion products, with an overall mass
9 balance dependent on user-specified species yields for major combustion species. To model
10 smoke movement, the user prescribes the smoke yield. A simple chemistry combustion scheme
11 in the model then determines the smoke particulate concentration in the form of an optical
12 density.

13 The results for CFAST and MAGIC are shown in Figure 5-33 and Figure 5-34 respectively. Only
14 the NIST/NRC tests have been used to assess predictions of smoke concentration. For these
15 tests, the smoke yield was specified as one of the test parameters. There are two obvious
16 trends in the results. First, the predicted concentrations are within or near experimental
17 uncertainties in the open-door tests. Second, the predicted concentrations are roughly three to
18 five times the measured concentrations in the closed-door tests. The experimental uncertainty
19 for these measurements has been estimated to be 19 percent.

20 The difference between model and experiment is far more pronounced in the closed-door tests.
21 Given that the oxygen and carbon dioxide predictions are no worse (and indeed even better) in
22 the closed-door tests, which might be because the smoke is not transported with the other
23 exhaust gases, either the specified smoke yield (which was developed from free-burning
24 experiments) is not appropriate for the closed-door tests or other phenomena are not accounted
25 for in the model. These qualitative differences between the open- and closed-door tests are
26 consistent with the FDS predictions.



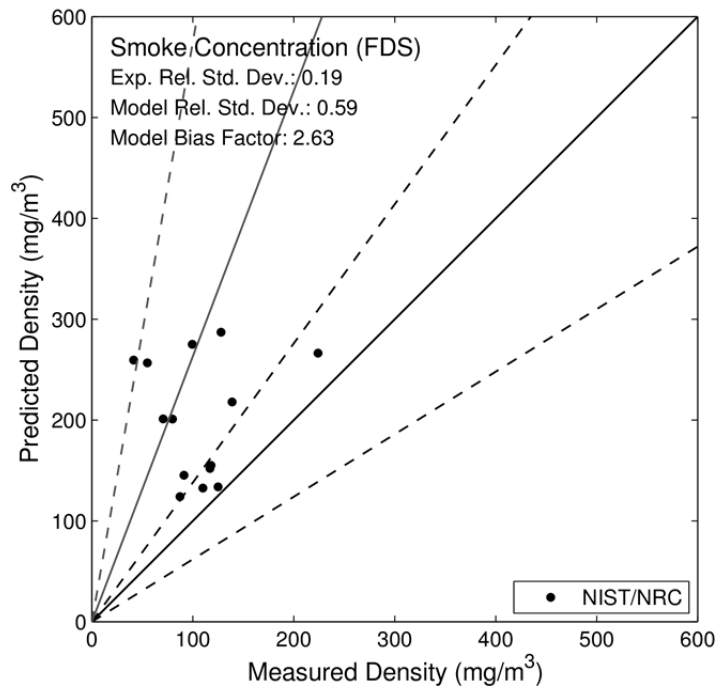
1
 2 **Figure 5-33. Smoke Concentration (CFAST).**



3
 4 **Figure 5-34. Smoke Concentration (MAGIC).**

VALIDATION RESULTS

- 1 CFD Model: The FDS results are shown in Figure 5-35. The FDS results show an
- 2 overestimation of the smoke concentration similar to that of the zone models. The
- 3 overestimation is most pronounced in the closed-door experiments of the NIST/NRC series.



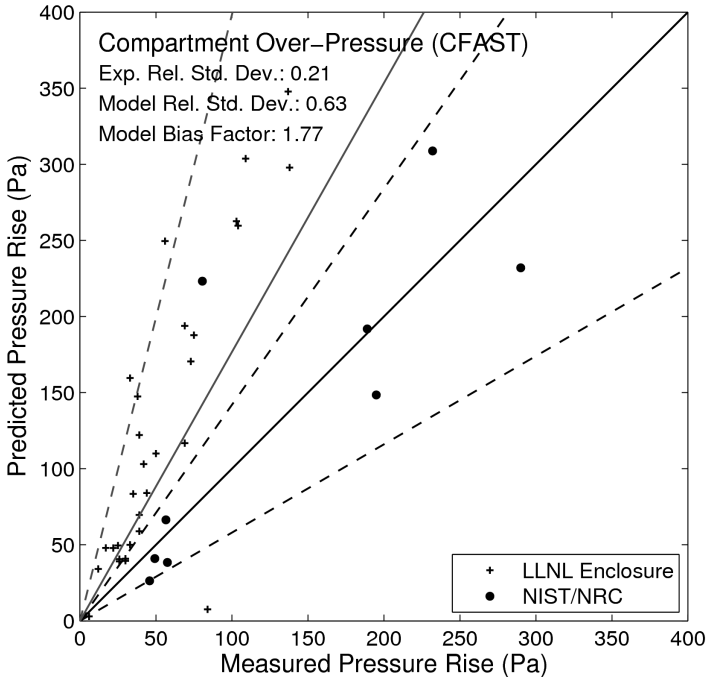
4
5 **Figure 5-35. Smoke Concentration (FDS).**

6 **5.2.7 Pressure**

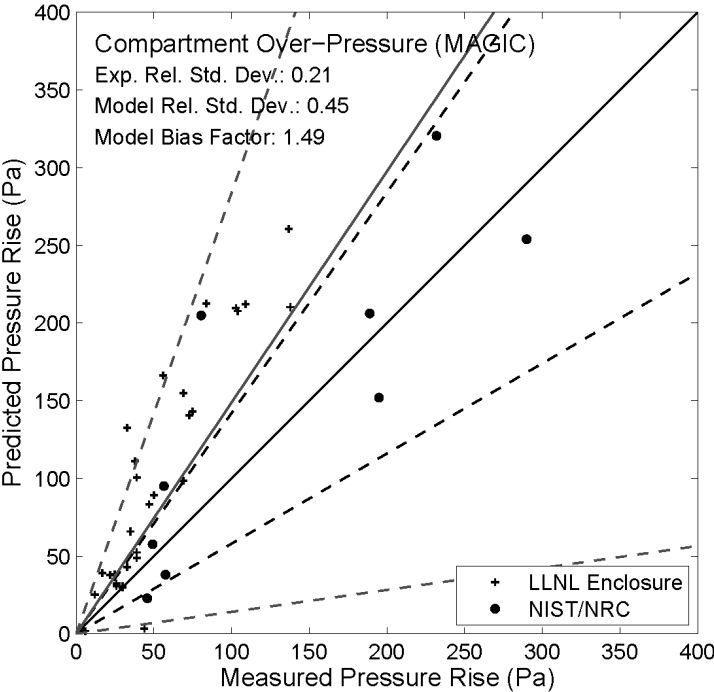
7 Room pressure is a rarely used quantity in NPP fire modeling. It might be important when it
8 contributes to smoke migration to adjacent compartments. Zone and CFD models calculate
9 room pressure as they solve energy and mass balance equations for individual compartments.
10 Empirical correlations only apply in the simplest of room geometries.

11 The measured pressures range from approximately 10 Pa to 300 Pa. The lower value is typical
12 of an open compartment; the higher value is typical of a closed compartment with leakage.

13 Zone Models: The results for CFAST and MAGIC are shown in Figure 5-36 and Figure 5-37
14 respectively. Prediction of pressure at a specific measurement point is particularly difficult for
15 zone models, which assume that pressure varies only as a function of height within a
16 compartment. The CFAST and MAGIC results are comparable and have a consistently higher
17 uncertainty than the FDS results.



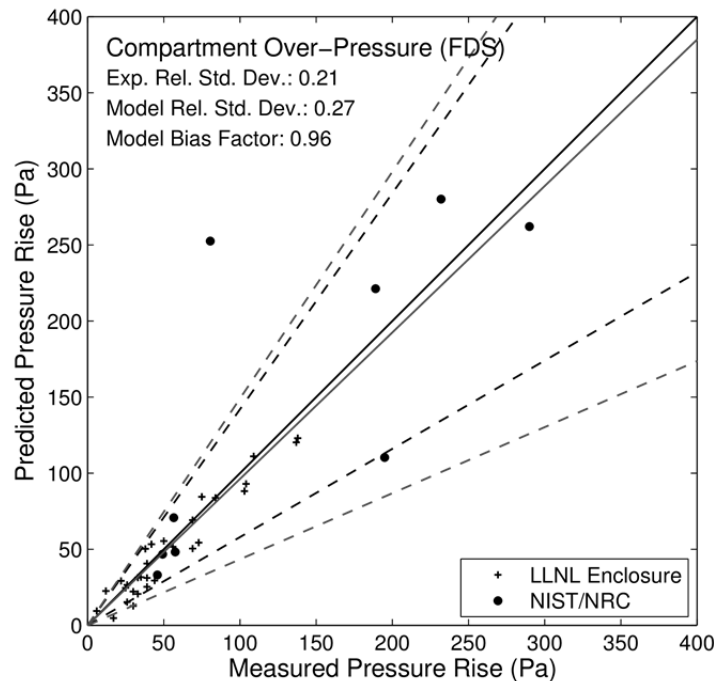
1
2 **Figure 5-36. Compartment Overpressure (CFAST).**



3
4 **Figure 5-37. Compartment Overpressure (MAGIC).**

VALIDATION RESULTS

- 1 CFD Model: The FDS results are shown in Figure 5-38; their accuracy is comparable to that of
- 2 the experimental measurements. This accuracy is based on the fact that FDS conserves mass
- 3 and energy globally, which along with basic thermodynamic principles assures that the overall
- 4 compartment pressure will be predicted reasonably well.



5
6 **Figure 5-38. Compartment Overpressure (FDS)**

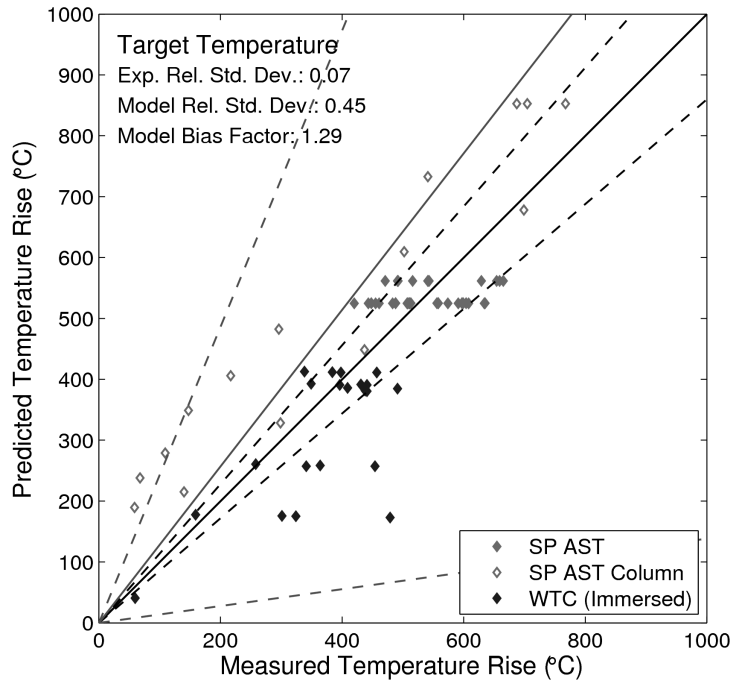
7 **5.2.8 Target Temperature**

8 The calculation of target temperature is perhaps the most common objective of fire-modeling
9 analyses. The zone and CFD models calculate the surface temperature of the target as a
10 function of time and consider the heat conducted into the target material.

11 The range of measured target temperatures varies from model to model because the simpler
12 models were not designed to address all of the target types and locations. The range of the
13 empirical and zone models extends to approximately 800 °C (1472 °F), while the CFD model
14 extends to about 1000 °C (1832 °F), where targets are fully immersed within a large
15 hydrocarbon fuel fire.

16 Empirical Correlations: The results for the empirical correlations are shown in Figure 5-39.
17 These targets include unprotected and protected steel members. HGL temperatures from the
18 MQH correlation were used as the exposing fire temperature for the SP AST and WTC
19 experiments; plume temperatures from the McCaffrey correlation were used as the exposing fire
20 temperature for the SP AST experiments. In the WTC experiments, the steel members were
21 both protected and unprotected, and only the steel members that were immersed in the HGL
22 were included because the specification of an exposing fire temperature is required. In the
23 protected steel cases, the empirical correlations use different heat transfer models that account

- 1 for the insulation material. The validation results do not include the NIST/NRC Experiments
- 2 because the empirical correlations assessed in this study do not address their scenario.

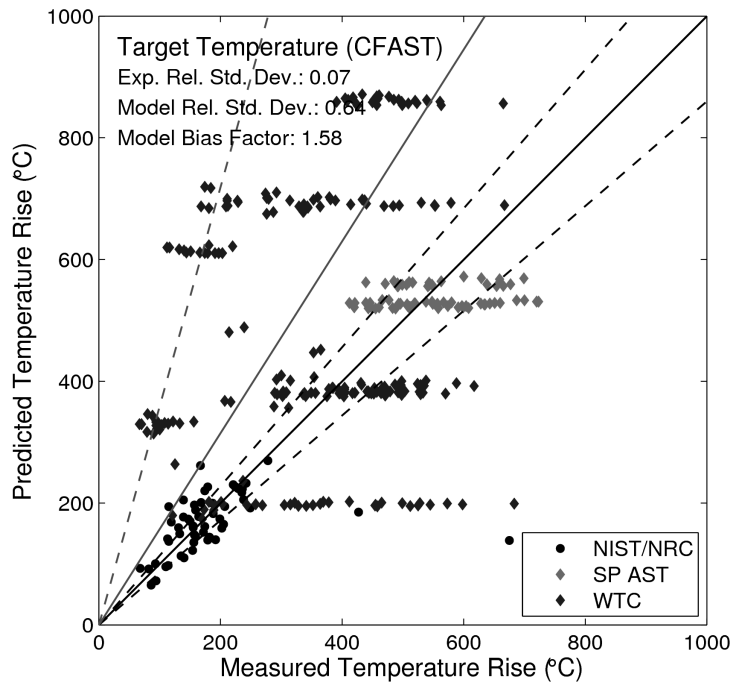


3
 4 **Figure 5-39. Target Temperature (Empirical Correlations)**

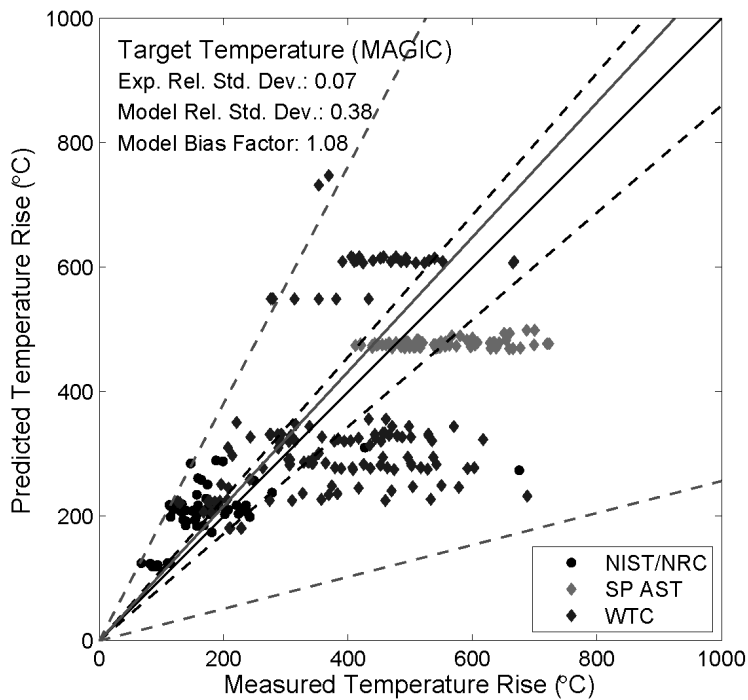
5 Zone Models: The results for CFAST and MAGIC are shown in Figure 5-40 and Figure 5-41
 6 respectively. The simplifying assumptions in a zone model are most evident in the prediction of
 7 inherently local conditions such as those on a target at a specific location in a compartment. For
 8 both zone models, bias and uncertainty are higher for target temperature and heat flux than for
 9 other quantities. Predictions for the NIST/NRC tests are often within experimental uncertainty,
 10 but predictions for the WTC tests, in which conditions were more extreme, show a far broader
 11 scatter.

12 Both models show a horizontal banding of predicted temperatures for tests that had numerous
 13 measurement points throughout a single compartment. This is typical of zone models for which
 14 the primary underlying assumption of two relatively uniform control volumes or layers within a
 15 compartment leads to relatively uniform predictions of target temperatures in the upper or lower
 16 layer. For measurement quite close to the ceiling, this banding is somewhat lessened because
 17 of the calculation of a ceiling-jet temperature; radiation from uniform surface temperatures
 18 adjacent to a layer also impact the calculation. The more spatially detailed calculations of a CFD
 19 model do not show this behavior. This assumption of uniform conditions within a layer also
 20 leads to some underprediction of temperature and heat flux for targets near the fire.

VALIDATION RESULTS

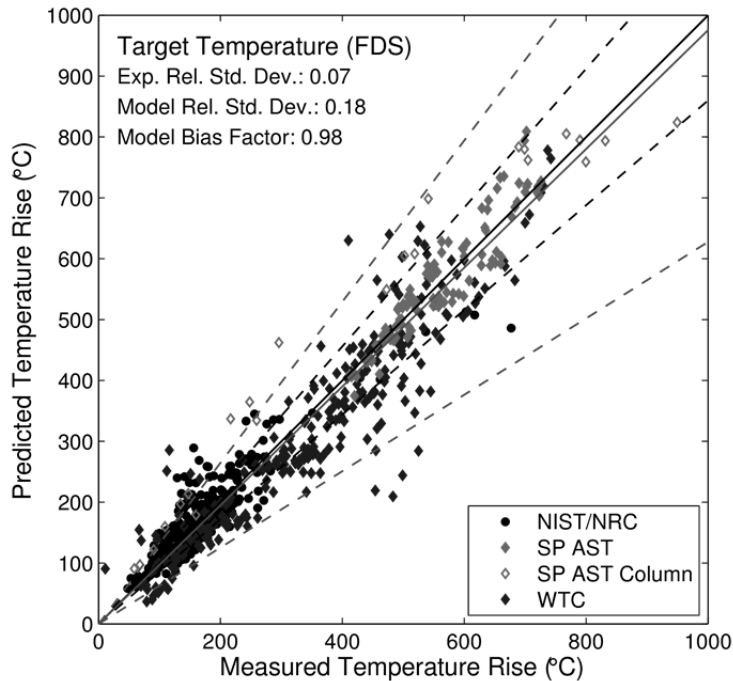


1
2 **Figure 5-40. Target Temperature (CFAST).**



3
4 **Figure 5-41. Target Temperature (MAGIC).**

1 CFD Model: The FDS results are shown in Figure 5-42. The FDS results show no obvious bias
 2 or trend. The targets include various types of electrical cables, steel beams, trusses, and
 3 columns. In the WTC experiments, the steel is both protected and unprotected. In cases
 4 involving protected steel, FDS calculates the heat penetration through the sprayed-on insulation
 5 material.



6
 7 **Figure 5-42. Target Temperature (FDS).**

8 **5.2.9 Target Heat Flux**

9 Thermal radiation and convection are important modes of heat transfer in fires. The models
 10 included in this study address heat flux with various levels of sophistication, from simply
 11 estimating flame radiation from a point source to solving the full radiation transport equation.
 12 The empirical models include simple estimates of flame radiation from a point or cylindrical
 13 source. Zone models include these same estimates and also include radiation exchange
 14 between hot and cold layers and surfaces. CFD models solve the radiation transport equation
 15 that predicts the gains and losses of thermal radiation from each individual gas and solid phase
 16 grid cell.

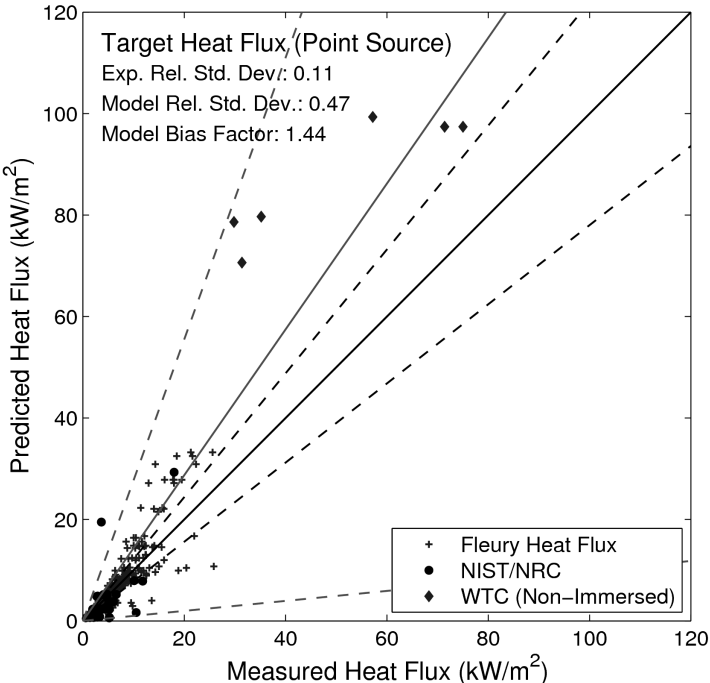
17 The measured heat fluxes range from nearly 0 kW/m² to nearly 120 kW/m². The empirical
 18 correlations cannot address all cases, however. For NPP applications, the ability to predict
 19 heat-flux values at the lower end of the scale is most important, because damage criteria for
 20 common electrical cable types (thermoplastic and thermoset) are 6 kW/m² and 11 kW/m² (see
 21 Table 8-2 in Volume 2 of NUREG/CR-6850 (EPRI 1011989)).

22 Empirical Correlations:

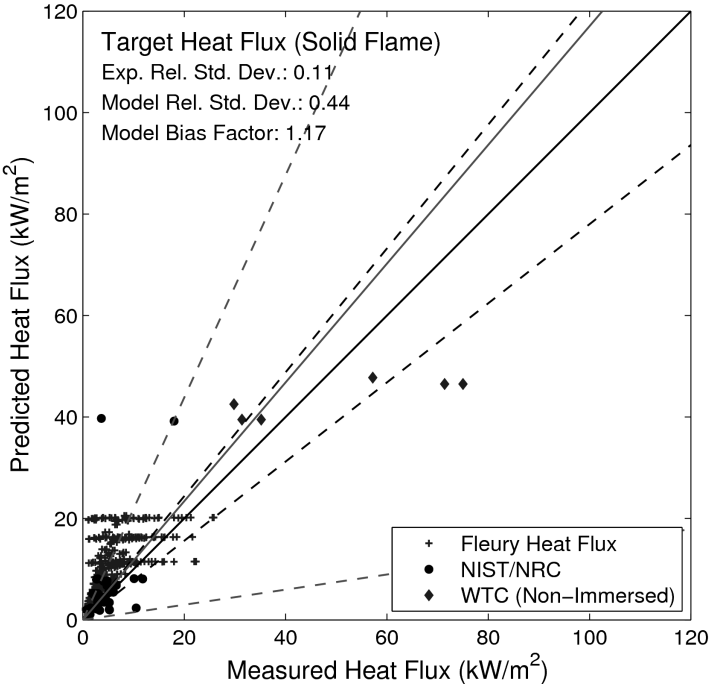
23 The results for the point-source radiation and solid-flame correlations are shown in Figure 5-43
 24 and Figure 5-44 respectively. Note that the point-source radiation model has higher uncertainty

VALIDATION RESULTS

- 1 for measurements closer to the flame, which is expected because the fire is represented as a
- 2 point source.
- 3 An attempt was made to include all of the experimental data from the WTC Experiments.
- 4 However, because some of the heat-flux gauges in the WTC Experiments were immersed in the
- 5 hot gas layer or plume, the radiation correlations significantly underpredicted the target heat flux
- 6 and the uncertainty was very large. Therefore, only heat flux gauges that were not immersed in
- 7 the hot gas layer or plume were included.



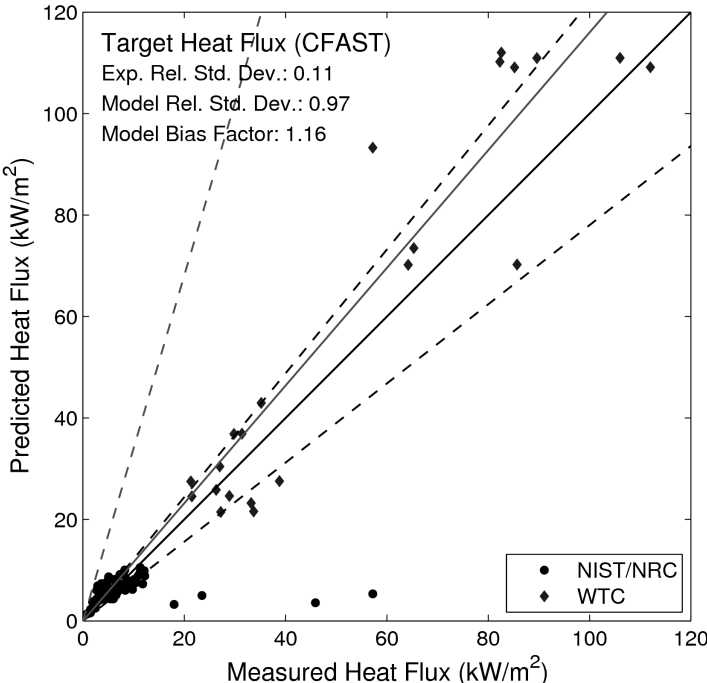
1
2 **Figure 5-43. Target Heat Flux (Point Source).**



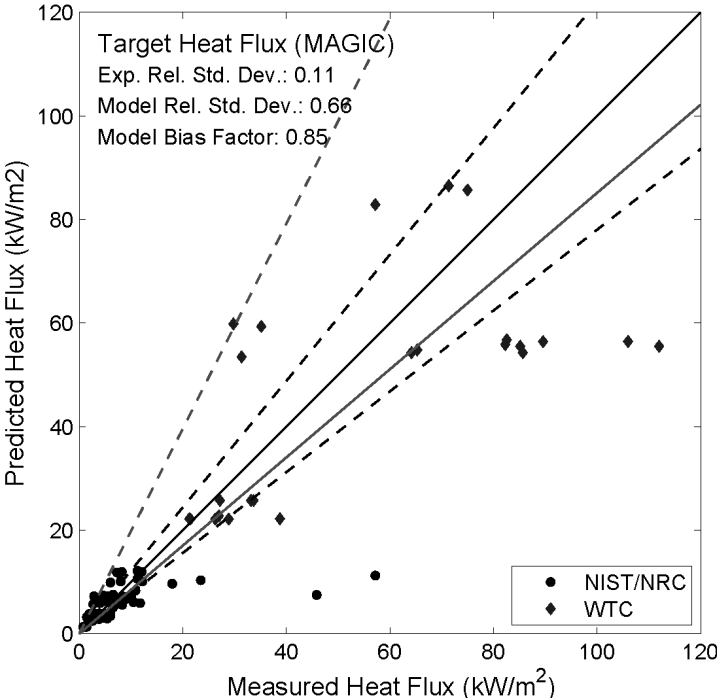
3
4 **Figure 5-44. Target Heat Flux (Solid Flame).**

VALIDATION RESULTS

1 Zone Models: The results for CFAST and MAGIC are shown in Figure 5-45 and Figure 5-46
2 respectively. Prediction of heat flux to targets and target surface temperature largely depends
3 on local conditions surrounding the target. Two zone models such as CFAST and MAGIC
4 predict an average representative value of gas temperature in the upper and lower regions of a
5 compartment. Thus, the models can be expected to underpredict values near a fire source and
6 overpredict values for targets remote from a fire. The uncertainty values for both models are
7 driven by a few outliers in the data. Note that the two points that are significantly underpredicted
8 in the NIST/NRC series are from a single experiment in which the fuel pan was moved close to
9 the heat flux gauges. This was done in several of the experiments, but only these two points
10 displayed a noticeable underprediction.



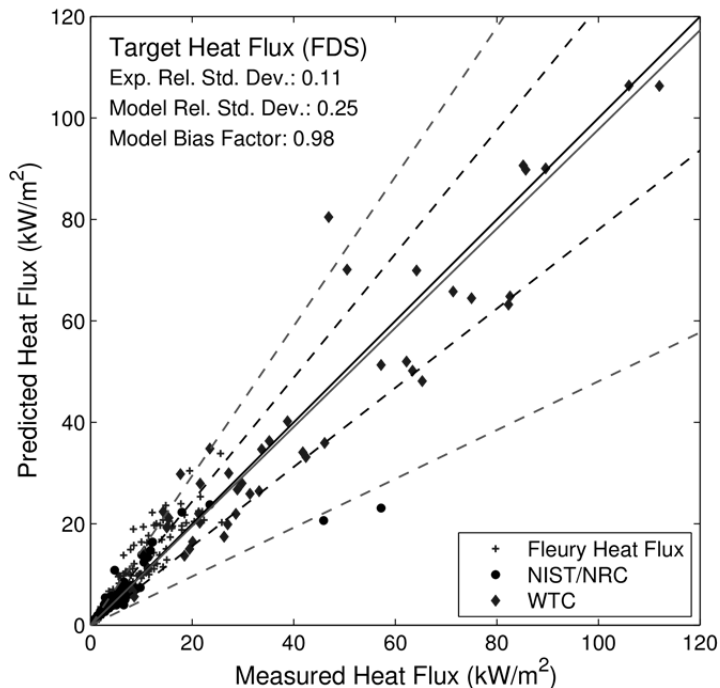
1
2 **Figure 5-45. Target Heat Flux (CFAST).**



3
4 **Figure 5-46. Target Heat Flux (MAGIC).**

VALIDATION RESULTS

1 CFD Model: The FDS results are shown in Figure 5-47. A large number of heat flux
2 measurements in the range from 1 kW/m² to 10 kW/m² dominate the bias and scatter of the
3 FDS predictions. However, the limited measurements at higher heat fluxes do not significantly
4 diverge from the trend indicated by the lower values. Note that the two points that are
5 significantly underpredicted in the NIST/NRC series are from a single experiment in which the
6 fuel pan was moved close to the heat-flux gauges. This was done in several of the experiments,
7 but only these two points displayed a noticeable underprediction.



8

9 **Figure 5-47. Target Heat Flux (FDS).**

10 **5.2.10 Surface Temperature**

11 Compartment surfaces include the compartment walls, ceiling, and floor. The empirical
12 correlations do not address the temperatures of the various compartment surfaces.

13 The range of measured surface temperatures extends to nearly 1000°C (1832°F), typical of
14 targets fully immersed in flames.

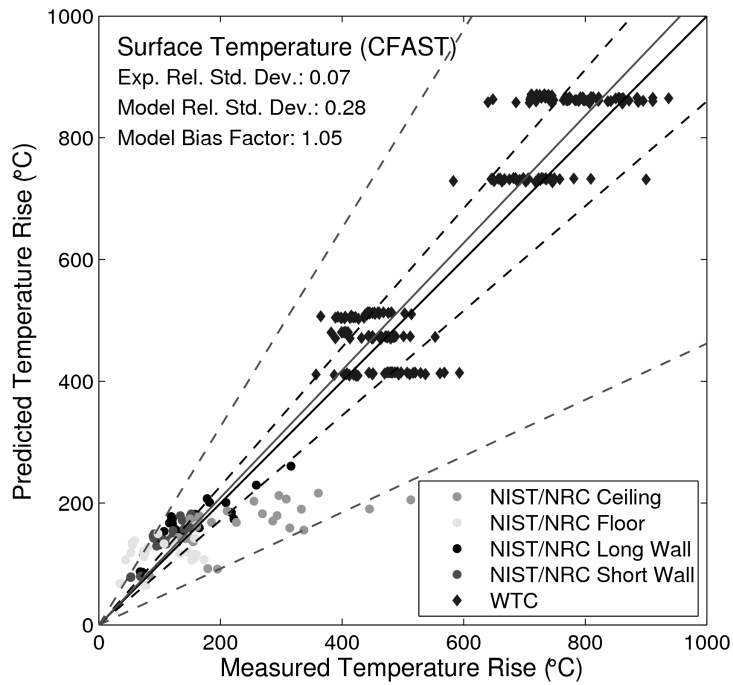
15 Zone Models: Surface temperatures for CFAST and MAGIC are shown in Figure 5-48 and
16 Figure 5-49, respectively. The models are capable of predicting the surface temperature of a
17 wall, assuming that its composition is fairly uniform and its thermal properties are well
18 characterized. Predictions are typically within 10 percent to 30 percent of the measured values.
19 Generally, the models overpredict the far-field fluxes and temperatures and underpredict the
20 near-field measurements. This is consistent with the single representative hot gas layer
21 temperature assumed by zone fire models. Both models show a horizontal banding of predicted
22 temperatures for tests which had numerous measurement points throughout a single
23 compartment. This is typical of zone models for which the primary underlying assumption of two
24 relatively uniform control volumes or layers within a compartment leads to relatively uniform

1 predictions of target temperatures in the upper or lower layer. For measurement quite close to
2 the ceiling, this banding is somewhat lessened because of the calculation of a ceiling-jet
3 temperature; radiation from uniform surface temperatures adjacent to a layer also impact the
4 calculation. The more spatially detailed calculations of a CFD model do not show this behavior.
5 This assumption of uniform conditions within a layer also leads to some underprediction of
6 temperature and heat flux for targets near the fire.

7 The uncertainty in the surface temperature predictions is particularly influenced by the
8 underprediction of ceiling surface temperatures. Both CFAST and MAGIC calculate a uniform
9 ceiling temperature enhanced by the presence of a ceiling jet. Still, the underlying weakness of
10 the zone model assumption of relatively uniform layer and surface temperatures becomes
11 especially apparent in the calculated ceiling temperatures for compartments where a fire is
12 located.

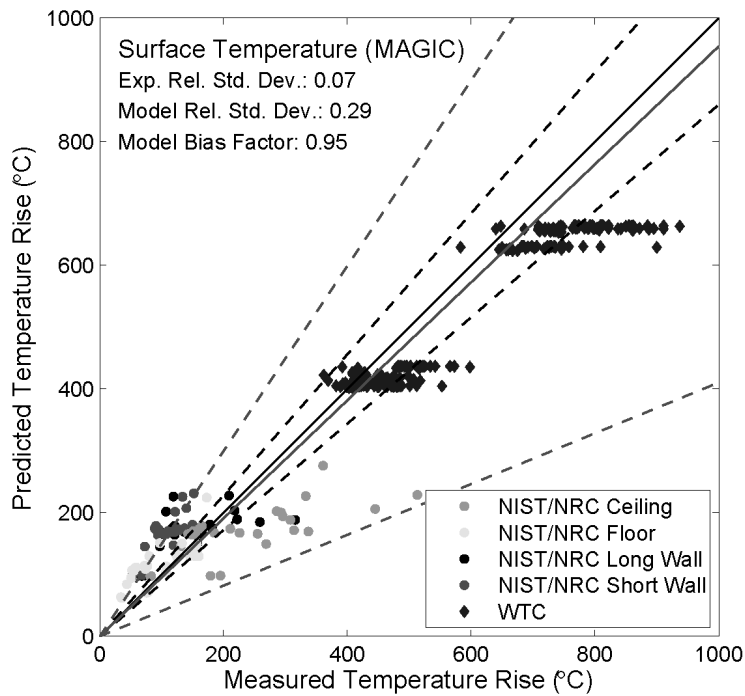
13 The wall temperatures and heat fluxes in MAGIC were calculated by placing individual targets in
14 the walls. The targets are characterized by the thermophysical properties and thickness of the
15 wall. This evaluation does not include either of MAGIC's output options "Wall Temperature" or
16 "Wall Heat Flux," which are available in the Wall output category. Experimental measurements
17 were compared with MAGIC's "Total Absorbed Heat Flux" output option.

VALIDATION RESULTS



1

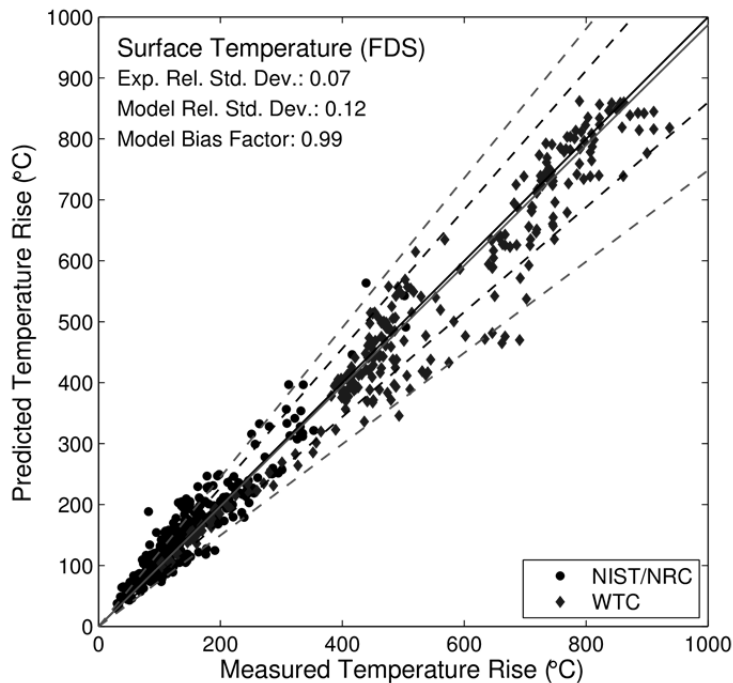
2 **Figure 5-48. Surface Temperature (CFAST).**



3

4 **Figure 5-49. Surface Temperature (MAGIC).**

1 CFD Model: The FDS results are shown in Figure 5-50. The FDS results indicate no particular
 2 trend or bias. The two sets of experiments considered included a large number of point
 3 measurements on all compartment surfaces. FDS treats all of these surfaces in the same way,
 4 except for a slightly different convective heat transfer coefficient depending on whether the
 5 surface is vertical or horizontal. The results do not indicate a greater or lesser degree of
 6 accuracy for either.



7
 8 **Figure 5-50. Surface Temperature (FDS).**

9 **5.2.11 Surface Heat Flux**

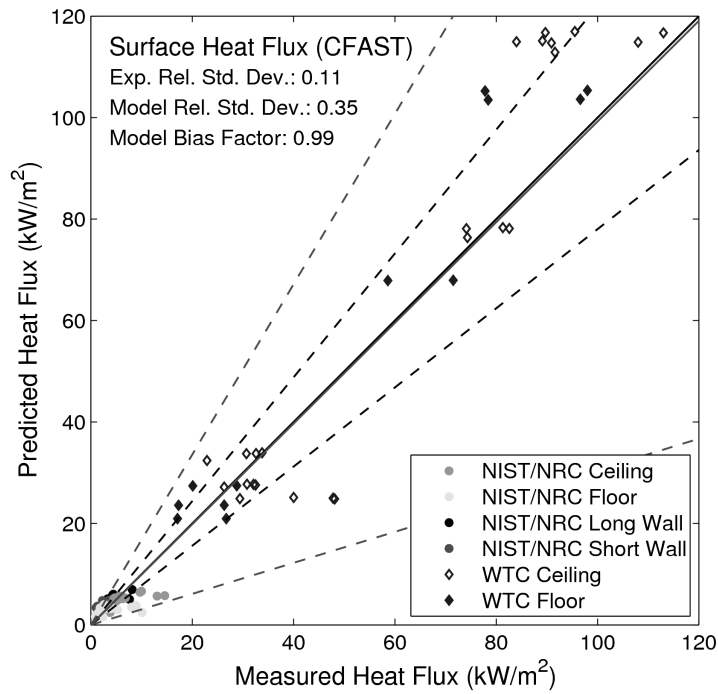
10 Surface heat flux is generally treated in the same manner as target heat flux, just as surface
 11 temperature is treated in the same manner as target temperature. In a CFD model, there are
 12 slight differences in the convective heat transfer coefficient, but in most cases, radiation heat
 13 transfer is the dominant model of surface heating.

14 The measured heat fluxes range from approximately 0 kW/m² to 120 kW/m². For NPP
 15 applications, predicted heat fluxes beyond 11 kW/m² suggest target damage; thus, the accuracy
 16 of the models is most important at the lower end of the range.

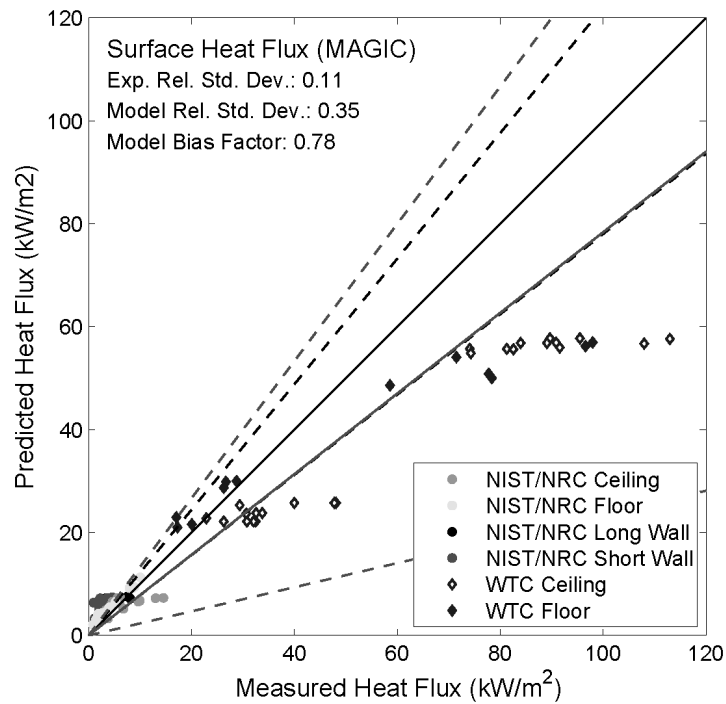
17 The empirical correlations do not address heat flux to various compartment surfaces.

18 Zone Models: The results for CFAST and MAGIC are shown in Figure 5-51 and Figure 5-52
 19 respectively. Trends similar to those for surface temperature predictions are seen in the surface
 20 heat flux predictions for the two zone models. Generally, the models overpredict far-field fluxes
 21 and temperatures and underpredict near-field measurements. This is consistent with the single
 22 representative hot gas layer temperature assumed by zone fire models. Both models also tend
 23 to somewhat underpredict ceiling temperatures and overpredict floor temperatures, likely
 24 because they both use the simple point source radiation algorithm for heat transfer from the fire.

VALIDATION RESULTS

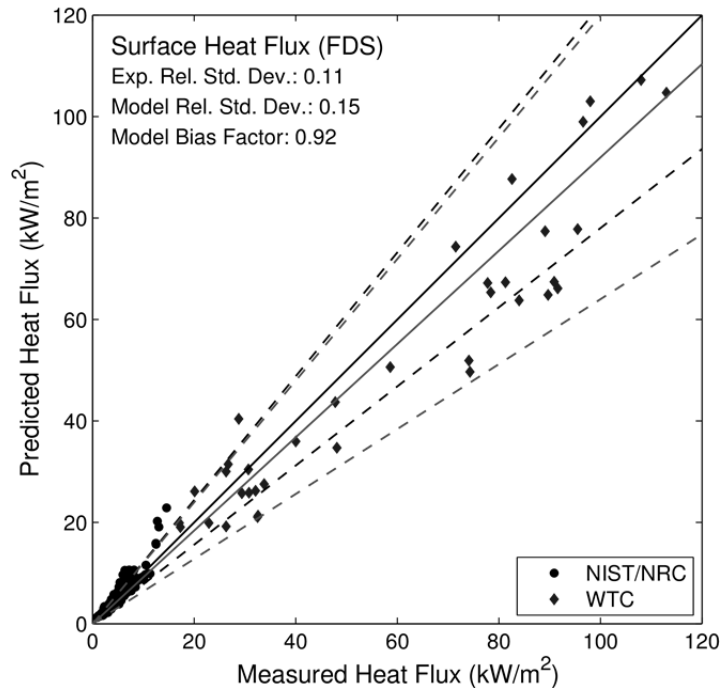


1
2 **Figure 5-51. Surface Heat Flux (CFAST).**



3
4 **Figure 5-52. Surface Heat Flux (MAGIC).**

1 **CFD Model:** The FDS results are shown in Figure 5-53. The FDS model uncertainty for the heat
 2 flux to walls, floors, and ceilings is based on data from two sets of experiments. In the
 3 NIST/NRC tests, most of the heat fluxes are relatively low because gauges were applied to
 4 surfaces that were remote from the fire. The purpose of these measurements was to assess the
 5 overall loss of energy from the entire compartment. The heat flux measurements in the WTC
 6 experiments, however, were made relatively close to the fire because the intent of the
 7 experiments was to assess the impact of a relatively large fire on structural elements and wall
 8 linings.



9
 10 **Figure 5-53. Surface Heat Flux (FDS).**

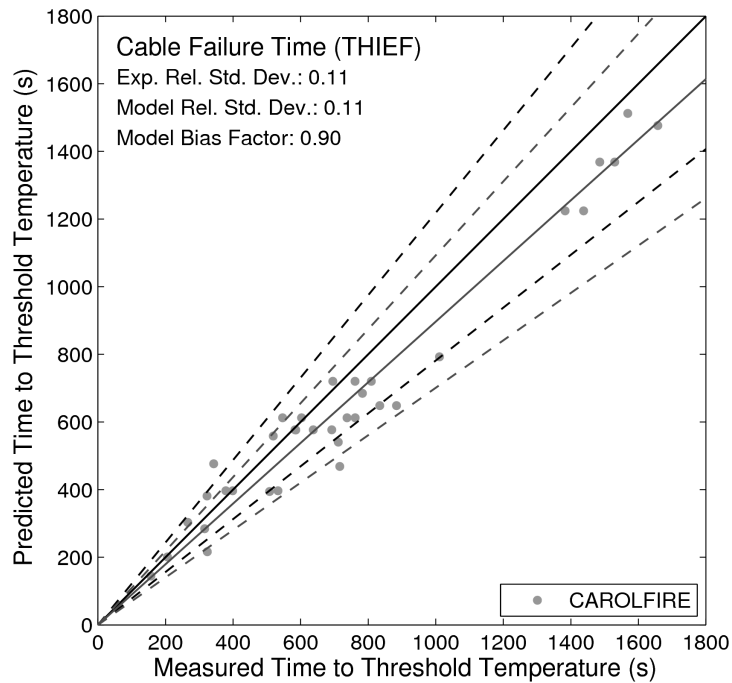
11 **5.2.12 Cable-Failure Time**

12 Even though an electrical cable is considered to be a “target,” a separate output quantity is
 13 included in this study to assess the models’ ability to predict the time to cable failure. This is an
 14 indirect way of assessing the models’ prediction of temperature. The models only predict the
 15 interior temperature of the cable, and the failure time is considered to be the time at which the
 16 predicted temperature rises above an experimentally determined value.

17 The THIEF model assumes that an electrical cable is a homogenous cylinder with constant
 18 values of specific heat and thermal conductivity and that the density is determined from its mass
 19 per unit length (McGrattan, 2008). The THIEF model has been implemented in various ways
 20 within the five fire models (FDT^s, FIVE-Rev2, CFAST, MAGIC, and FDS) discussed in this
 21 report. Both the FDT^s and FIVE-Rev2 have standalone implementations; the other three models
 22 use implementations appropriate to the type of model. The user’s guide for each model should
 23 be reviewed for details concerning the respective implementation.

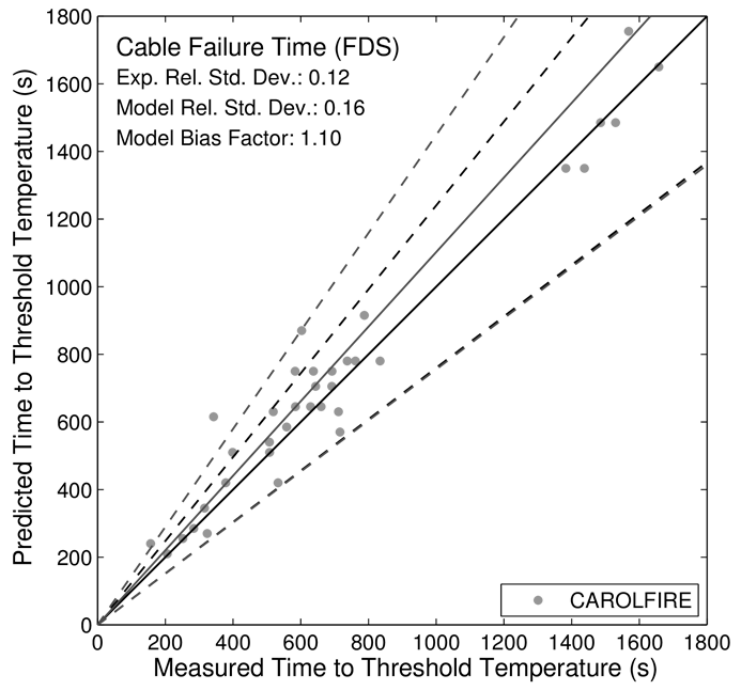
VALIDATION RESULTS

- 1 The measured failure times range from a few minutes to nearly a half hour. The longer failure
- 2 times are typical of cables protected by steel conduit.
- 3 Standalone THIEF Model: The THIEF model has been implemented in FDT^s and THIEF's
- 4 predictions of the CAROLFIRE experiments are shown in Figure 5-54.



- 5
- 6 **Figure 5-54. Cable-Failure Time (THIEF).**

- 7 THIEF Model within a CFD Model: The FDS results are shown in Figure 5-55. The THIEF model
- 8 is implemented in FDS. It differs from the FDT^s version only in that FDS predicts the
- 9 time-varying gas temperature and heat flux to the cable surface. For example, the CAROLFIRE
- 10 experimental apparatus was modeled in FDS to better predict the thermal environment
- 11 surrounding the cable target.



1
 2 **Figure 5-55. Cable Failure Time (FDS).**

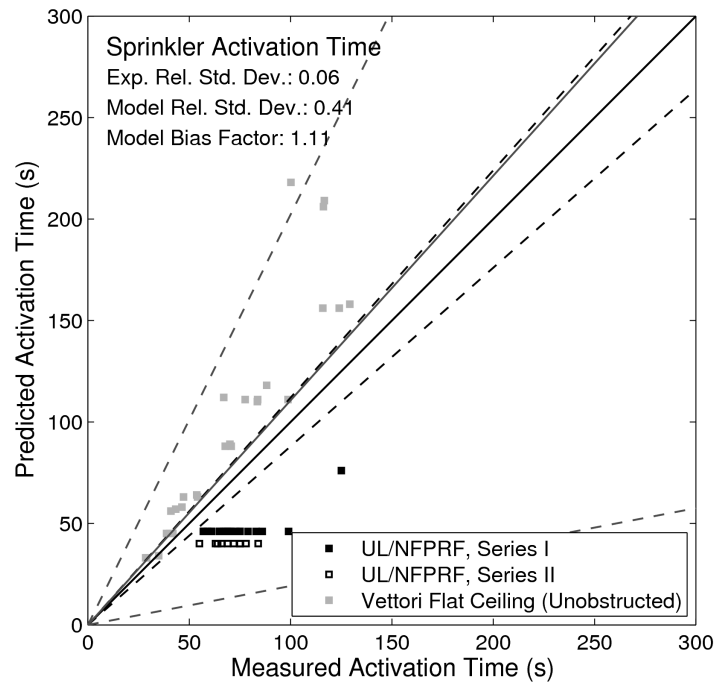
3 **5.2.13 Sprinkler Activation Time**

4 Much like an electrical cable, a sprinkler is merely a “target” with a particular set of thermal
 5 properties, such as the response time index (RTI) that indicates the sensitivity of the sprinkler’s
 6 fusible link or glass bulb. Activation is assumed to occur when the link or bulb reaches a
 7 predetermined threshold temperature.

8 The experiments range from relatively small residential sprinklers in the Vettori experiments to
 9 relatively large industrial sprinklers in the UL/NFPRF experiments. The basic physics of both
 10 scenarios are mostly the same. Note that an extra set of experiments, the “Vettori Sloped
 11 Ceiling” experiments, was conducted by Vettori at NIST. The results of those experiments were
 12 only compared to those of FDS because none of the other models have the ability to model a
 13 sloped ceiling.

14 Empirical Correlation: The results for the Alpert correlation are shown in Figure 5-57. The
 15 empirical correlations can only predict ceiling jet flows for the simplest geometries. For this
 16 reason, for the Vettori experiments, only a subset of the experimental data (from tests with a
 17 smooth, horizontal, and unobstructed ceiling) was included.

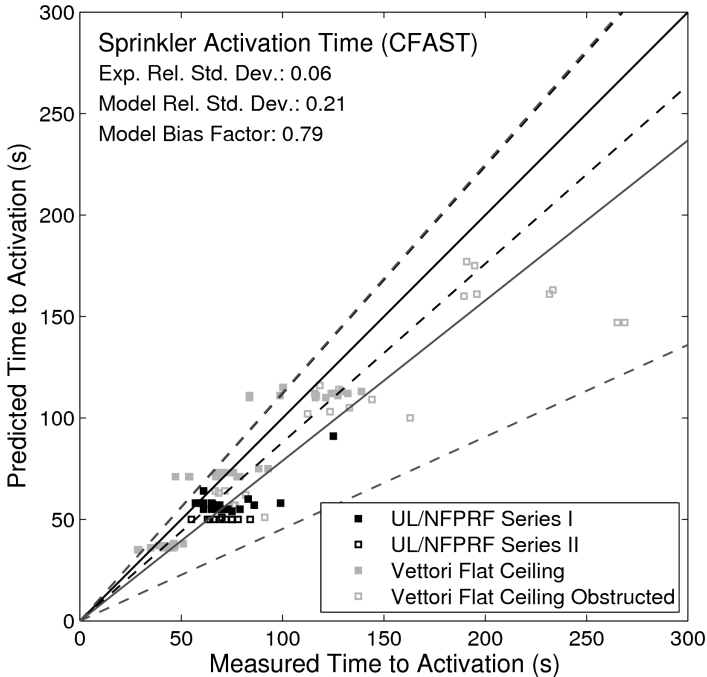
VALIDATION RESULTS



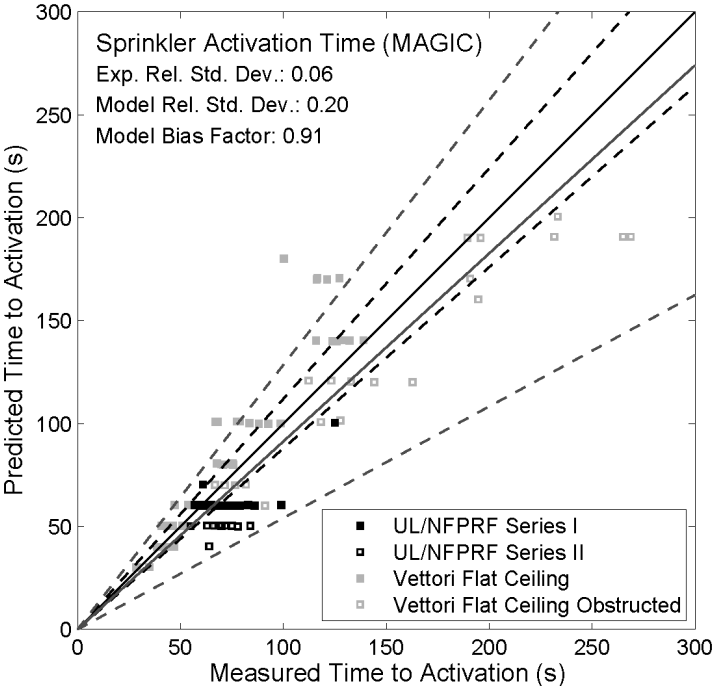
1

2 **Figure 5-56. Sprinkler Activation Time.**

3 Zone Models: Sprinkler activation times for CFAST and MAGIC are shown in Figure 5-57 and
4 Figure 5-58 respectively. The results from the two models are similar but not identical. In
5 general, CFAST predicts activation times somewhat shorter than those of MAGIC, particularly
6 for the obstructed ceiling cases in the Vettori flat ceiling test series. The difference is likely
7 caused by different assumptions in the two models for the gas temperature surrounding the
8 sprinkler. Although both models use an RTI based calculation of heat transfer to the sprinkler,
9 CFAST uses the ceiling jet gas temperature while MAGIC uses the (typically somewhat cooler)
10 temperature of the hot gas layer, leading to longer activation times for MAGIC.



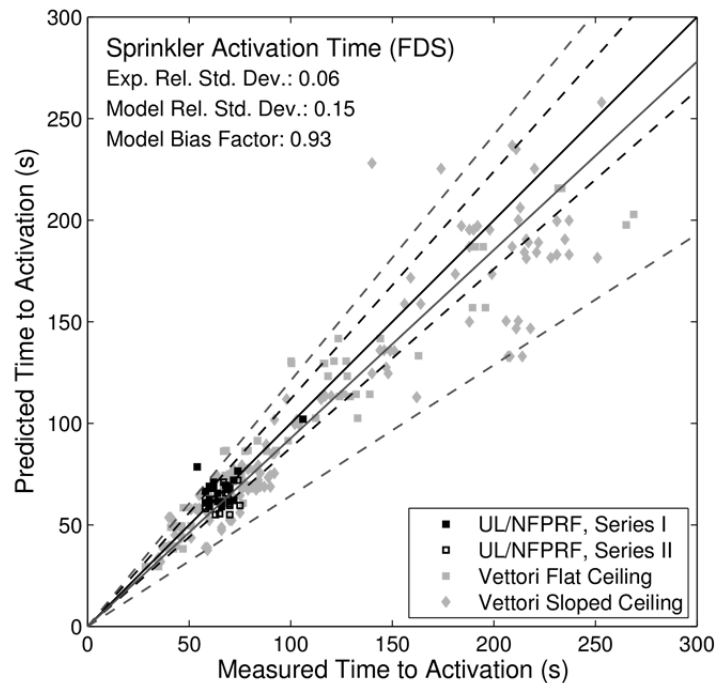
1
2 **Figure 5-57. Sprinkler Activation Time (CFAST).**



3
4 **Figure 5-58. Sprinkler Activation Time (MAGIC).**

VALIDATION RESULTS

1 CFD Model: The FDS results are shown in Figure 5-59. FDS underpredicts sprinkler activation
2 time by about 7 percent. Note that data from both Vettori's flat- and sloped ceiling experiments
3 are included. The zone and empirical models do not have the ability to model a sloped ceiling.
4 FDS models a sloped ceiling as a series of stair-stepped obstructions. There appears to be a
5 greater degree of model uncertainty associated with the more challenging sloped ceiling
6 experiments.



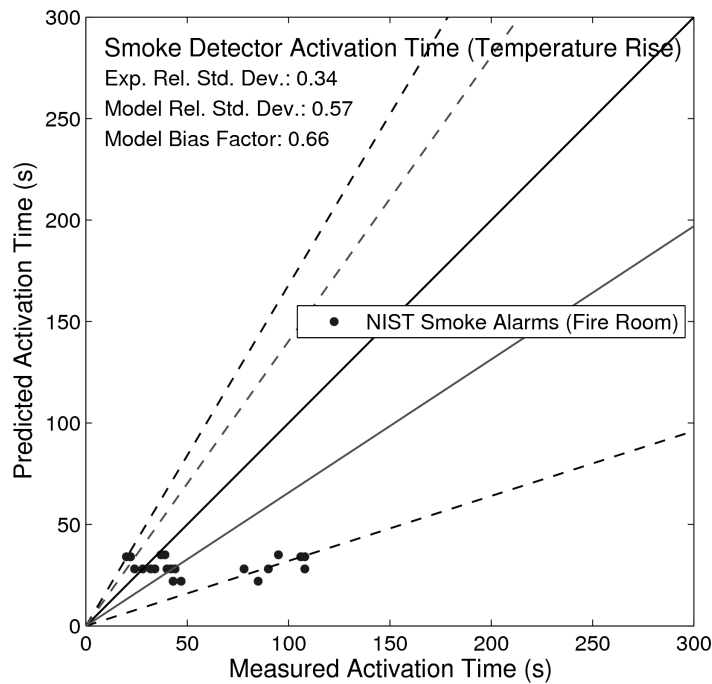
7
8 **Figure 5-59. Sprinkler Activation Time (FDS).**

9 **5.2.14 Smoke Detector Activation Time**

10 Smoke detectors can be modeled in a variety of ways. A popular method is to assume that the
11 detector behaves like a very sensitive sprinkler with a low activation temperature and RTI. CFD
12 models such as FDS have an alternative approach in which the smoke concentration and gas
13 velocity in the vicinity of the detector is predicted and a simple time-lag equation is solved to
14 account for the transport of smoke into the sensing chamber. This latter approach requires a set
15 of empirical parameters that characterize the particular geometry of the device. The former
16 approach typically treats all detectors as the same by using fixed values of activation
17 temperature and RTI. In this validation study, only one set of data is used, from the NIST Home
18 Smoke Alarms experiments. These experiments involved seven different types of detectors, but
19 none of the time-lag parameters required by the alternative approach were provided in the test
20 report. Therefore, all of the models below use the simple temperature rise approach with fixed
21 values of activation temperature and RTI.

22 Empirical Correlations: The results for smoke detector activation time using the low RTI, low
23 temperature rise assumption are shown in Figure 5-60. The temperature and velocity of the
24 gases near the detector are predicted using the Alpert ceiling jet correlation, and the activation
25 time is predicted under the assumption that the smoke detector responds like a sprinkler with an

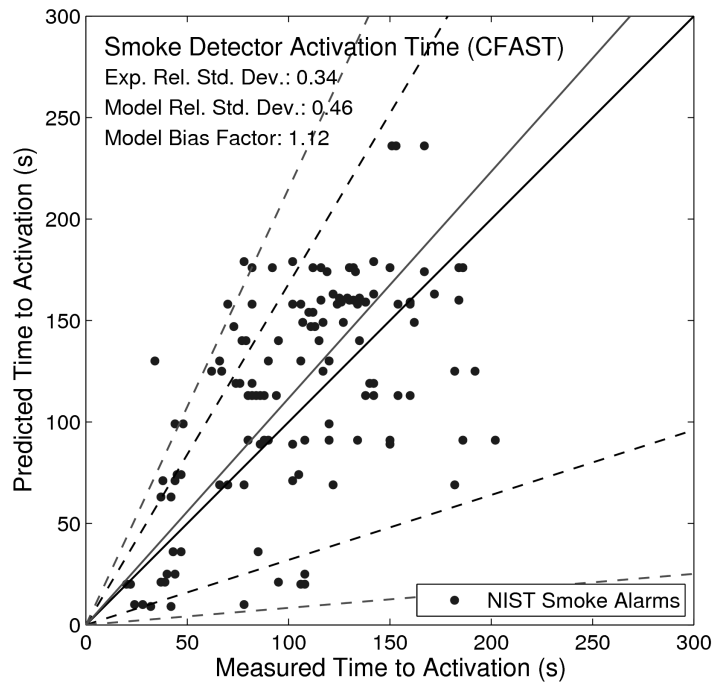
- 1 RTI of $5 \text{ (m}\cdot\text{s)}^{0.5}$ and activation temperature of $5 \text{ }^\circ\text{C}$ above ambient. Note that only the smoke
- 2 detectors that were located in the fire room of the NIST Smoke Alarms Experiments were
- 3 included because the Alpert ceiling jet correlation cannot account for multiple rooms.



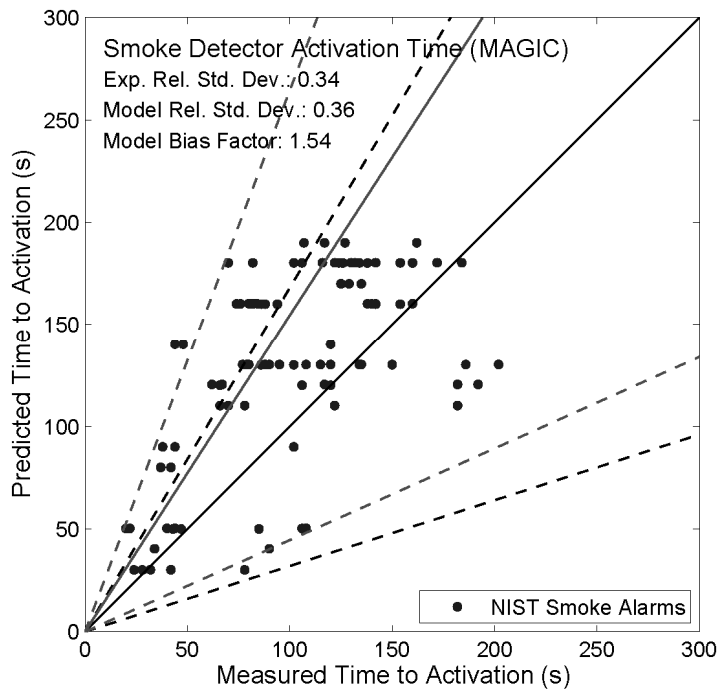
4
 5 **Figure 5-60. Smoke-Detector Activation Time (Temperature Rise).**

6 Zone Models: The results for CFAST and MAGIC are shown in Figure 5-61 and Figure 5-62
 7 respectively. Like its predictions of the sprinkler activation times, CFAST’s predictions of smoke
 8 alarm activation time tend to be a bit shorter than those of MAGIC. Both models treat smoke
 9 alarms in the same manner as heat detectors and sprinklers, with a fixed activation temperature
 10 ($5 \text{ }^\circ\text{C}$ above ambient temperature) and RTI (a value of $5 \text{ (m s)}^{1/2}$). As with sprinkler activation,
 11 CFAST uses the ceiling jet gas temperature while MAGIC uses the (typically somewhat cooler)
 12 temperature of the hot gas layer, leading to typically longer activation times for MAGIC.

VALIDATION RESULTS

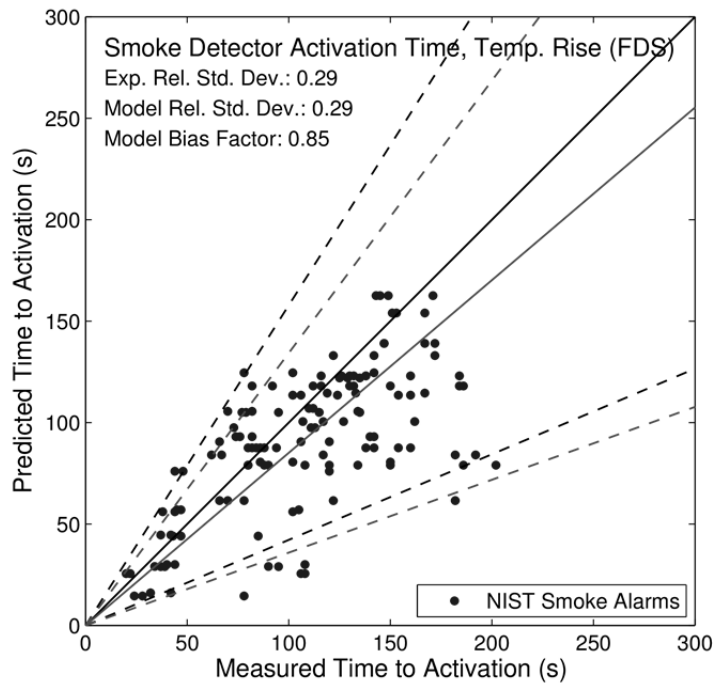


1
2 **Figure 5-61. Smoke Detector Activation Time (CFAST).**



3
4 **Figure 5-62. Smoke Detector Activation Time (MAGIC).**

1 CFD Model: The FDS results are shown in Figure 5-63. FDS can model smoke detector
 2 activation time either by assuming that the detector acts like a sprinkler with a low RTI or by
 3 calculating the time for the smoke concentration to reach an alarm threshold within the detector.
 4 For the latter method, FDS requires several parameters that characterize the lag time and
 5 activation concentration. For the NIST Smoke Alarms experiments, these parameters are not
 6 provided; thus, FDS uses the same temperature-rise algorithm as the empirical and zone
 7 models. Note that the experimental and model uncertainty values are 0.29 rather than 0.34, as
 8 reported in subsection 3.3.3, because the calculation of the model uncertainty does not allow a
 9 value less than the experimental uncertainty.



10
 11 **Figure 5-63. Smoke Detector Activation Time (FDS).**

12

1 **5.3 Summary of Validation Results**

2 Table 5-1 summarizes the results of this validation study. As discussed in Section 5.1, the
3 predictive capabilities of the models are assessed based on the quantitative values of relative
4 difference between model prediction and experimental measurements.

5 Note that the values in Table 5-1 are based on the versions of the models listed in Section 1.3.
6 These values do not apply to earlier versions of the models. In particular, the model-accuracy
7 metrics that were cited in NUREG-1934 (EPRI 1023259) in 2012 are based on earlier versions
8 of the models.

9 In general, the CFD model, FDS, is the most accurate, followed by the zone models, followed by
10 the empirical correlations. This is to be expected because CFD models are more faithful to the
11 underlying physics, but they also require hours or days to complete calculations that can be
12 done in less than a minute by the other models.

13 There are some exceptions to the general hierarchy of models. For example, FDS is of
14 comparable accuracy to the zone models in predicting plume temperatures. This is not
15 surprising because the zone models use well established empirical correlations of plume
16 temperatures, whereas FDS predicts these temperatures by solving the governing fluid flow
17 equations. At best, FDS should predict comparable temperatures.

18 The zone and CFD models all overpredicted smoke concentration by approximately a factor of
19 three, possibly because the models do not account for smoke losses to the walls and ceiling.

20 The zone models are relatively accurate in predicting the average HGL temperature, but less
21 accurate in predicting localized surface temperatures and heat flux.

22

1 **Table 5-1. Summary of model-uncertainty metrics.**

Output Quantity	Empirical Correlations			CFAST		MAGIC		FDS		Exp
	Corr.	δ	$\tilde{\sigma}_M$	δ	$\tilde{\sigma}_M$	δ	$\tilde{\sigma}_M$	δ	$\tilde{\sigma}_M$	$\tilde{\sigma}_E$
HGL Temp. Rise, Natural Ventilation	MQH	1.17	0.15	1.20	0.36	1.13	0.30	1.02	0.12	0.07
HGL Temp. Rise, Forced Ventilation	FPA	1.29	0.32	1.15	0.19	1.08	0.17	1.21	0.22	0.07
	DB	1.18	0.25							
HGL Temp. Rise, No Ventilation	Beyler	1.04	0.37	1.00	0.08	1.07	0.16	1.20	0.12	0.07
HGL Depth	ASET/YT	-	-	1.05	0.34	1.17	0.31	1.03	0.06	0.05
Ceiling Jet Temp. Rise	Alpert	0.86	0.11	1.16	0.39	1.04	0.45	0.98	0.14	0.07
Plume Temp. Rise	Heskestad	0.84	0.33	1.07	0.20	1.04	0.20	1.20	0.21	0.07
	McCaffrey	0.90	0.31							
Oxygen Concentration	N/A			1.00	0.15	0.93	0.22	1.01	0.11	0.08
Smoke Concentration	N/A			3.69	0.68	3.71	0.66	2.63	0.59	0.19
Pressure Rise	N/A			1.77	0.63	1.49	0.45	0.96	0.27	0.21
Target Temp. Rise	Steel	1.29	0.45	1.58	0.64	1.08	0.38	0.98	0.18	0.07
Target Heat Flux	Point Source	1.44	0.47	0.97	1.16	0.85	0.66	0.98	0.25	0.11
	Solid Flame	1.17	0.44							
Surface Temp. Rise	N/A			1.05	0.28	0.95	0.29	0.99	0.12	0.07
Surface Heat Flux	N/A			0.99	0.35	0.78	0.35	0.92	0.15	0.11
Cable Failure Time	THIEF	0.90	0.11	-	-	-	-	1.10	0.16	0.12
Sprinkler Activation Time	Sprinkler	1.11	0.41	0.79	0.21	0.91	0.20	0.93	0.15	0.06
Smoke Detector Act. Time	Temp. Rise	0.66	0.57	1.12	0.46	1.54	0.36	0.85	0.29	0.34

2

VALIDATION RESULTS

1 **Notes:**

2 Experiments that had compartments with ceiling vents, high wall vents, multi-story
3 configurations, irregular geometry, or complex wall materials were not included in the evaluation
4 of the empirical correlations for HGL temperature.

5 There was insufficient data to derive the uncertainty statistics for the ASET/YT correlation.

6 Refer to subsection 5.2.3 for an explanation of the use of Alpert's correlation in unconfined vs.
7 compartment scenarios.

8 The evaluation of the empirical correlations for Target Heat Flux only included targets that were
9 not immersed in the hot gas layer or plume.

10 The evaluation of the empirical correlations for Sprinkler Activation Time only included sprinklers
11 that were located on a smooth, horizontal, and flat ceiling.

12 The evaluation of the empirical correlation for Smoke Detector Activation Time only included
13 detectors located in the room of origin.

14

15

16

6

CONCLUSION

This study provides further justification for verification and provides validation through comparisons between experimental data and predictions for the most current versions of the five fire-modeling tools used in the nuclear industry.

The most current versions of all five models have been verified by this study as appropriate for fire-protection applications, within the assumptions for each individual model or sub-model. The project team used guidance in ASTM E1355 about the theoretical basis and mathematical and numerical robustness to make this determination.

The validation results are presented in the form of a relative bias factor and standard deviation for each of the predicted quantities that are considered important for nuclear power-plant (NPP) fire-modeling applications. These accuracy metrics are based on the relative differences between model predictions and applicable experimental measurements. The predictive capability considers the uncertainty in the experimental measurements. The following observations are based on review of these results and generally apply to the five fire models considered in this study:

1. The results of this study apply only to the versions of the models listed in Section 1.3. These results cannot be applied to earlier versions of the models. NUREG-1934 (EPRI 1023259) contains results from earlier versions of these models.
2. The experiments considered in this study represent configurations that are typical of NPP applications. Not all possible NPP scenarios have been evaluated in this study. For a variety of reasons, experimental data is limited. Users should evaluate independently whether the results of this study are applicable to their specific scenario. Table 3-3 provides guidance in this matter.
3. For the fire scenarios considered in the current validation study, and for the output quantities of interest, the libraries of empirical correlations (FDT^s, FIVE) have fewer capabilities than the zone models or FDS. The correlations that the libraries contain are typically empirically deduced from a broad database of experiments. The correlations are based on fundamental conservation laws and have gained a considerable degree of acceptance in the fire-protection engineering community. However, because of their empirical nature, these correlations should be used within their limits of applicability.
4. The zone models, CFAST and MAGIC, predict global quantities like HGL temperature, HGL depth, and compartment pressure well, but are less accurate than FDS in predicting localized quantities such as ceiling-jet and surface temperatures and heat flux. This is expected given that zone models are designed to predict average quantities.
5. In general, FDS is more accurate than the empirical and zone models. However, for certain quantities, such as plume temperature rise in the absence of a hot gas layer, empirical and zone models should provide comparable accuracy because they are based on time-averaged experimental measurements whereas FDS must compute the time-dependent fluid dynamics directly.
6. The decision to use any of these models depends on many considerations. Real fire scenarios rarely conform neatly to some of the simplifying assumptions inherent in the models. Although engineering calculations and two-zone models can be applied in instances

CONCLUSION

1 in which the physical configuration is complex, their accuracy cannot be ensured. CFD
2 model predictions can be more accurate in more of these complex scenarios. However, the
3 time it takes to get and understand a prediction might also be an important consideration in
4 the decision to use a particular model for a specific scenario. FDS is computationally
5 expensive and, while the zone models produce answers in seconds to minutes, FDS
6 provides comparable answers in hours to days. FDS is better suited to predict fire
7 environments within more complex configurations because it predicts the local effects of a
8 fire.

9 7. Like all predictive models, the best predictions come with a clear understanding of the
10 limitations of the model and of the inputs provided to do the calculations. The bias factor and
11 standard deviation values listed in Table 5-1 can be applied to the results of a given fire
12 model's prediction as uncertainty bounds. This uncertainty should be combined with
13 uncertainty in the various user-selected input parameters.

14

7

REFERENCES

- 3 NOTE: Reference entries use the names of the organizations that were in effect when the document
4 was published. Keep in mind that the American Society for Testing and Materials is now
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10. SUPPLEMENTARY NOTES

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11. ABSTRACT (200 words or less)

There is a movement to introduce risk informed and performance based (RI/PB) analyses into fire protection engineering practice, both domestically and worldwide. This movement exists in both the general fire protection and the nuclear power plant (NPP) fire protection communities. The U.S. Nuclear Regulatory Commission (NRC) has used risk informed insights as part of its regulatory decision-making since the 1990s. In 2001, the National Fire Protection Association (NFPA) issued the 2001 Edition of NFPA 805, "Performance Based Standard for Fire Protection for Light Water Reactor Electric Generating Plants." In July 2004, the NRC amended its fire protection requirements in Section 50.48, "Fire Protection," of Title 10, "Energy," of the Code of Federal Regulations to permit existing reactor licensees to voluntarily adopt fire protection requirements contained in NFPA 805 as an alternative to the existing deterministic fire protection requirements. One key tool needed to further the use of RI/PB fire protection is the availability of verified and validated (V&V) fire models that can reliably predict the consequences of fires. In 2007, the NRC, together with the Electric Power Research Institute (EPRI) and the National Institute of Standards and Technology (NIST), conducted a research project to verify and validate five fire models that have been used for NPP applications. The results of this effort were documented in a seven volume report, NUREG 1824 (EPRI 1011999), "Verification and Validation of Selected Fire Models for Nuclear Power Plant Applications." This supplement expands on the previous V&V effort and evaluates the latest versions of the five fire models including additional test data for validation of the models.

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