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M. O. MEDFORD  
MANAGER, NUCLEAR LICENSING

TELEPHONE  
(818) 302-1749

May 1, 1986

Director, Office of Nuclear Regulation  
Attention: Mr. George E. Lear, Director  
PWR Project Directorate No. 1  
U. S. Nuclear Regulatory Commission  
Washington, D. C. 20555

Gentlemen:

Subject: Docket No.1 50-206  
Requests for Additional Information  
San Onofre Nuclear Generating Station  
Unit 1

- References:
1. Letter, George E. Lear, NRC, to Kenneth Baskin, SCE, Request for Additional Information, March 25, 1986
  2. Letter, Richard F. Dudley, NRC, to Kenneth P. Baskin, SCE, San Onofre Unit 1, April 21, 1986.
  3. Letter, Richard F. Dudley, NRC, to Kenneth P. Baskin, SCE, San Onofre Unit 1, April 29, 1986.
  4. Letter, M. O. Medford, SCE, to A. E. Chaffee, NRC, Investigation Report of November 21, 1985 Water Hammer Event, April 8, 1986

References 1, 2 and 3 requested additional information needed to review information provided to the NRC in meetings and in the SCE Investigation Report provided by Reference 4. The SCE Investigation Report identified three areas where further information would be provided to the NRC by April 30, 1986. Additionally, numerous telephone calls have occurred between SCE and the NRC Staff to clarify, respond to, or discuss new issues resulting from the review of the November 21, 1985 event. Accordingly, find enclosed the information necessary to resolve the issues raised to date.

The following listing describes the contents of the enclosures.

- Enclosure 1 - Provides responses to the questions transmitted by Reference 1.
- Enclosure 2 - Provides responses to the questions transmitted by Reference 2.
- Enclosure 3 - Provides responses to the questions transmitted by Reference 3.

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Mr. G. E. Lear

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May 1, 1986

Enclosure 4 - Provides the information deferred in Reference 4 to April 30, 1986.

If you have any questions, please let me know.

Very truly yours,

*M. D. Medford*

cc: Mr. J. B. Martin, Regional Administrator, NRC, Region V  
Mr. A. E. Chaffee, Regulatory Projects Branch, Region V  
Mr. Gary Zech, Office of Inspection and Enforcement  
Mr. F. R. Huey, NRC Senior Resident Inspector, SONGS 1, 2 & 3

ENCLOSURE 1

RESPONSES TO MARCH 25, 1986 LETTER

ATTACHMENT 1

1965 HEAT BALANCE

QUESTION NO. 1

System Design/Operating Data

- a. At steady state 92% rated thermal power (RTP), what are the feed flows (in lb/hr and gpm), pressures, and temperatures encountered at the feed pump discharge check valves (12") and the steam generator feed line check valves (10")? How was this data obtained?
- b. What were the above data at steady state 100% RTP? How was the data obtained?
- c. What is the minimum steady state flow rate, along with pressures and temperatures, that these valves encounter?
- d. Clearly indicate the source and reliability of the Atwood Morrill valve data used in the redesign calculations.

RESPONSE

- a. Using plant operating data based on station logs at 92% RTP extrapolated to the check valve locations, the values are:

	<u>12" Valves</u>	<u>10" Valves</u>
Flow (lb/hr)	$2.5 \times 10^6$	$1.67 \times 10^6$
Flow (gpm)	5600	3952
Temperature °F	332 (Note 1)	405 (Note 3)
Pressure (psia)	1080 (Note 2)	710 (Note 4)

- Notes: 1. Based upon an increase of 2°F through feed pump (typical from 1965 heat balances).
2. Based upon a 10 psi pressure drop through 1st Point Feedwater Heater (obtained from station manual) and a 10 psi drop through the piping up to control valve.
3. Based upon 2°F temperature drop from first point heater to check valve.
4. Based on calculated 350 psi pressure drop across control valve ( $C_v \approx 200$ ).

- b. The flows, temperatures and pressures at 100% RTP for the subject valves are:

	<u>12" Valves</u>	<u>10" Valves</u>
Flow (lb/hr)	$2.85 \times 10^6$	$1.90 \times 10^6$
Flow (gpm)	6425	4533
Temperature °F	339	416 (Note 1)
Pressure (psia)	995 (Note 2)	620 (Note 2)

The data was obtained from the original calculated heat balance diagram M20-5687889-3 (Attachment 1).

Notes: 1. Assumes approximately 2<sup>o</sup>F temperature drop from first point heater to check valve.

2. Pressures are approximate based on pump curves.

c. The expected minimum flows, pressures and temperatures are provided below. The flow for 10" check valves uses the minimum main feedwater flow control valve position of 5% as the basis. The flow for the 12" check valves uses the feedwater pump minimum flow as the basis.

	<u>12" Check Valves</u>	<u>10" Check Valves</u>
Flow (gpm)	700	200
Pressure (psia)	1,150	760
Temperature ( <sup>o</sup> F)	220	260

d. Atwood-Morrill calculated pressure drop values were provided in their letter of February 20, 1986 (Attachment 2). Valve testing recently performed on one 10" check valve provided actual pressure drop under the modeled conditions. Both the calculated value and test results indicate pressure drops under 1 psi for low flow operation and in the 2-4 psi range under full flow conditions.

STEAM GENERATOR

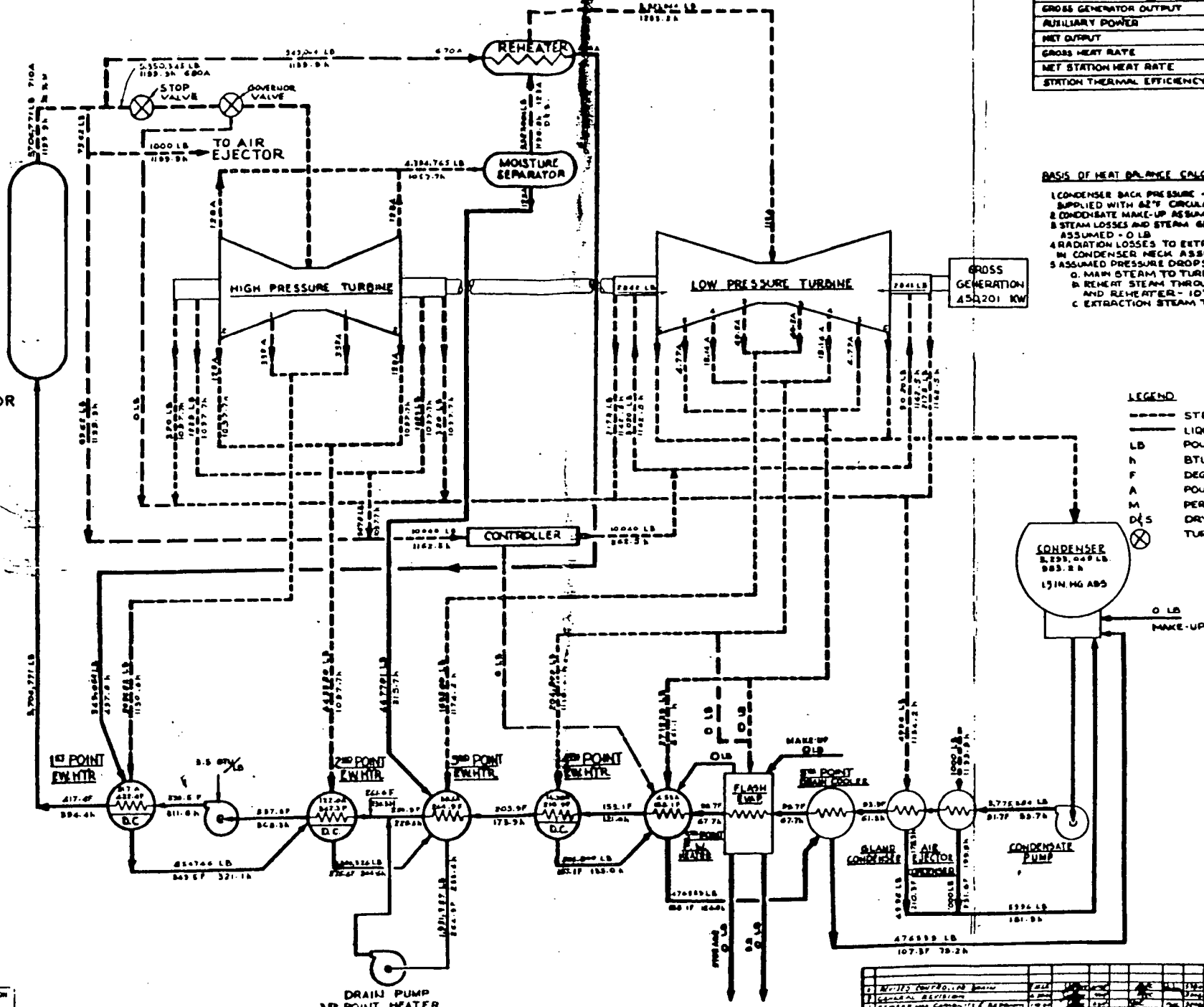
PERFORMANCE	
GROSS GENERATOR OUTPUT	450,201 KW
AUXILIARY POWER	KW
NET OUTPUT	KW
GROSS HEAT RATE	BTU/KWH: 10,211
NET STATION HEAT RATE	BTU/KWH
STATION THERMAL EFFICIENCY	%

**BASIS OF HEAT BALANCE CALCULATIONS:**

- CONDENSER BACK PRESSURE - 15" HG ABSOLUTE WHEN SUPPLIED WITH 82°F CIRCULATING WATER.
- CONDENSATE MAKE-UP ASSUMED - 0 LB.
- STEAM LOSSES AND STEAM GENERATOR BLOWDOWN ASSUMED - 0 LB.
- RADIATION LOSSES TO EXTRACTION PIPING LOCATED IN CONDENSER NECK ASSUMED - 0 BTU/HR.
- ASSUMED PRESSURE DROPS:
  - MAIN STEAM TO TURBINE STOP VALVE 30PSI
  - REHEAT STEAM THROUGH MOISTURE SEPARATOR AND REHEATER - 10%
  - EXTRACTION STEAM TO FW HEATERS - 5%

**LEGEND**

- STEAM LINES
- LIQUID LINES
- LB POUNDS PER HOUR
- H BTU PER POUND
- F DEGREES FAHRENHEIT
- A POUNDS PER SQ. IN. ABSOLUTE
- M PERCENT OF MOISTURE
- D/S DRY AND SATURATED
- ⊗ TURBINE VALVES



REVISIONS	
1	INITIAL DESIGN
2	REVISED DESIGN
3	REVISED DESIGN
4	REVISED DESIGN
5	REVISED DESIGN
6	REVISED DESIGN
7	REVISED DESIGN
8	REVISED DESIGN
9	REVISED DESIGN
10	REVISED DESIGN

BECHTEL CORPORATION  
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M 20-568789-3

ATTACHMENT 2

ATWOOD-MORRILL LETTER DATED 02/20/86





**ATWOOD & MORRILL CO. INC.**  
DESIGNERS AND MANUFACTURERS SINCE 1800

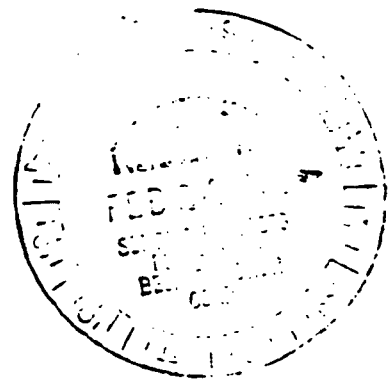
285 CANAL STREET • SALEM, MASSACHUSETTS 01970 • PHONE 617 744-5690 • TELEX 94-0299

February 20, 1986

Bechtel Power Corporation  
12440 East Imperial Highway  
Norwalk, CA 90650

Attention: Mr. Fred Lizmi

Subject: San Onofre  
Check Valve Position Indicators  
Bechtel P.O. Nos. VB200603  
VB200611  
A&M S.O. No. 15487



Dear Fred:

The following information is provided to confirm or clarify my previous discussions with Craig Walsh.

1. The reference dimensions on from the certified drawing (6.69", 8.50" and 10.94" for the 4", 10" and 12" valves, respectively) show the as cast ID of these valve bodies at the valve inlet and outlet. This small ID allows us to use the same castings for a variety of pipe sizes and pipe schedules. For your valves, this small ID is completely machined out so that the inlet and outlet are as shown on the weld end details and the minimum port size through these valves is as shown on previous correspondence.

The certified drawings will be changed, removing these reference dimensions as requested.

2. For local position indication, we propose to extend a small diameter shaft through one of the bearing covers as shown on the attached sketch. With this arrangement a pointer attached to the small diameter shaft will rotate with the disc/disc arm indicating valve position.

We propose to use a small diameter shaft in lieu of a full diameter shaft to minimize the packing friction in the stuffing box. It is our design philosophy that the packing friction on a full size shaft would be so high that there would be a danger of preventing valve movement.

3. The calculated water velocity through the seat and the pressure drop through each 10" valve is as shown below. These calculation are based on the water density of 49 lbs/cubic foot.

Flow Rate	Seat Velocity (ft/sec)	Delta P (psi)
1,830,000 lb/hr	28	2.6
4200 GPM	25	2.0
165 GPM	1	0.6
25 GPM	0.2	0.6

Please note that the velocities at 165 and 25 GPM are far below the minimum recommended velocities and that the pressure drops for these velocities are at best crude estimates. A better calculation for these pressure drops could be done only at a price increase.

Intermittent operation for short periods of time under these low flow conditions is, of course, permissible. However, this is severe service for a check valve and we would expect the valve disc to repeatedly open and bang closed.

We trust this information is satisfactory. If you have any questions, please contact us.

Very truly yours,

ATWOOD & MORRILL CO., INC.

  
John T. Mahoney  
Senior Sales Engineer

JTM/ko  
JTM23

c: M. Macdonald - A&M

Robert Burns & Associates, Inc.  
Attn: Robert Burns

QUESTION NO. 2

Valve Technical and Performance Requirements

- a. What was the design basis for the 10" and 12" valves in terms of flows, port size, obturator weights, pressure, and temperatures for both the MCC-Pacific and Atwood-Morrill valves? How does this differ from actual values?
- b. What are the acceptable operating ranges for the new valves and what is the impact on plant/system operations?
- c. What are the maintenance, installation, and operation requirements or guidelines provided by MCC-Pacific and Atwood-Morrill?
- d. Will the new valves be modified to include operator assists or position indicators?
- e. What are the "enhanced" surveillance and maintenance requirements and their basis for the Atwood-Morrill valves? Are they from or concurred by the manufacturer?
- f. What are the Atwood-Morrill bonnet and packing torque values?
- g. Where is the Atwood-Morrill actual hinge and disc combination center of gravity?

RESPONSE

- a. The design process conditions for the flow, temperature and pressure for the lines in which the 10" and 12" valves are installed is presented in Attachment 1. The 100% load 1965 data would apply to the MCC-Pacific valves and the 92% data applies to the Atwood-Morrill valves.

The port size is selected by the supplier. The MCC-Pacific design basis was originally based on the 100% data and is now subject to the 92% conditions.

- b. Performance tests by Dr. J. Paul Tullis and Dr. William J. Rahmeyer of Utah State University Foundation have provided operating ranges for the San Onofre Unit 1 feedwater check valves. The test results showed the Atwood-Morrill check valves are acceptable for all of the tested operating ranges at the locations downstream of the feed pumps and control valves and the proposed locations inside containment. These flow ranges are:

10" Valves	Up to 4267 gpm
12" Valves	Up to 6000 gpm

- c. Atwood-Morrill has provided an instruction manual detailing the maintenance and installation requirements and procedures for their valve (Attachment 2). Operational guidelines are being developed as explained in the response to Question 2e. The original maintenance procedures provided by MCC-Pacific could not be located. The current operation and maintenance manuals is provided as Attachment 3.
- d. No operator assists or position indicators will be included on the valves.

Due to the fact that the Atwood-Morrill valve has a 20° seat angle, the arc of travel required from full open to full close is much shorter than typical swing check valves. This allows the valve to seat quickly upon flow reversal, therefore, operator assists are not required. The addition of position indicators requires, by nature, a bore and accompanying shaft seal in the valve body. This seal can lead to two significant complications, the first of which is the possibility of seal leakage. The other is the friction force of the seal on the hinge shaft. This force can inhibit valve closure and thus increase the severity of a possible water hammer event. Also, performance tests of the valve have not shown any need for operator assists. A final consideration is given in the A-M instruction manual (Attachment 2, page 3) which states, "For valves with . . . no outside lever or air closing cylinder, preventative maintenance is minimal."

- e. Test procedure guidelines have been issued for leak rate testing of critical feedwater and auxiliary feedwater check valves (Attachment 4). SCE is developing test procedures for surveillance testing and maintenance of check valves from these guidelines. These surveillance procedures have not been issued to date. The surveillance leak rate limits have been calculated based upon limiting the steam admission to the feedwater piping. No supplier review or concurrence is required for the surveillance leak rate limits.
- f. The Atwood-Morrill value has no packing and the bonnet is a pressure seal type. However, there are bolts on the bonnet to hold in the pressure seal. Atwood-Morrill has provided a bolt-torque table (Attachment 2, page 7), a portion of which is shown below.

<u>Valve</u>	<u>Bolt Size</u>	<u>Required Bolt Stress</u>	<u>Required Bolt Torque</u>
4"	5/8 - 11	25,000 psi	50 ft-lb
10"	7/8 - 9	25,000 psi	142 ft-lb
12"	7/8 - 9	25,000 psi	142 ft-lb

- g. The center of gravity for the hinge/disc combination for the 4", 10" Schedule 60 and Schedule 80, and 12" valves are located as shown in the sketch provided by Atwood-Morrill (Attachment 5).

ATTACHMENT 1

PROCESS CONDITIONS AT 100% AND 92% RTP

Plant Condition Data	100% Load (1965)		92% Load	
	10" Valves	12" Valves	10" Valves	12" Valves
Flow (lb/hr)	1.90 x 10 <sup>6</sup>	2.85 x 10 <sup>6</sup>	1.67 x 10 <sup>6</sup>	2.50 x 10 <sup>6</sup>
Flow (gpm)	4533	6425	3952	5600
Temperature (°F)	416	339	405	332
Pressure (psia)	620	995	710	1080

NOTE: See responses to Questions 1a and 1b for explanation of the basis for this data.

ATTACHMENT 2

ATWOOD-MORRILL INSTRUCTION MANUAL

INSTRUCTION MANUAL

FOR

FREE FLOW REVERSE CURRENT VALVES  
DOUBLE BEARING COVER DESIGN

Manufactured by  
Atwood & Morrill Co., Inc.  
Salem, Massachusetts

Bechtel P.O. No. V8200603  
Atwood & Morrill S.O. No. 15487

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DOCUMENT STATUS <input checked="" type="checkbox"/> Manufacturer may proceed <input type="checkbox"/> Exceptions as noted. Make changes and resubmit. Manufacturer may proceed. <input type="checkbox"/> Correct and resubmit. <input checked="" type="checkbox"/> Information only. <input type="checkbox"/> Distribution required.	DATE <b>3/5/86</b>
PF-1218 (10070) 8/82	

<input checked="" type="checkbox"/> This revised Vendor Document incorporates changes associated with a Design Change Package (DCP). DCP Number <b>3400.-</b>
<input type="checkbox"/> This Vendor Document revision does not reflect any physical plant modification and is not associated with a DCP or FCR.
Explain change
Reviewed by <b>P. CLUZ</b> Date <b>3/5/86</b>
PI-6183 (10070) 5/83

501-408-1-2-8-0



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Valve Dwg. No. 15487-05	
Valve Dwg. No. 15487-06	

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SECTION I  
GENERAL INFORMATION

Application

The check valve purpose is to prevent a reversal of flow, and consists of a swinging disc so arranged that when the flow enters the valve from the inlet end, the disc pivots on its shaft, swinging upward to allow a free flow through the valve. As flow diminishes disc will pivot downward toward its seat. If flow stops or if a reversal of flow occurs, the disc will seat and seal, preventing a reversal of flow through the protected system.

Construction

The valve is a straight-through type having a swinging disc rotating on a heavy shaft in bushed bearings with a pressure sealed bonnet or bolted bonnet. The combination disc and disc arm are of cast steel to guard against breakage. The shaft rides in nitrided stainless steel bushings. Shaft is sealed at each end by a bearing cover, using a flexitallic gasket. This construction eliminates end thrust as both ends of the internal shaft are subject to the same pressures.

Valve Operation - Normal

The check valve will protect against reverse flow through the section of the system where it is installed.

The valve is a free swinging, gravity closing type check valve. The valve disc will open when the inlet pressure becomes slightly higher than the outlet pressure and will close when the inlet pressure becomes slightly less than the outlet pressure or a reversal of flow occurs.

SECTION II  
INSTALLATION

The valve is connected to the line by butt welding or bolting through the valve flange and the pipe flange.

The valves are delivered by the manufacturer in a clean, dry condition free of grease, slag or other foreign matter. All openings are sealed to prevent the entry of any foreign matter into the valve during shipment. These seals should not be removed until just before the valve is installed.

Inspect the valve carefully for evidence of damage in transit.

After the valve has been installed, cycle it several times to be sure it functions properly.

## MAINTENANCE

PREVENTIVE MAINTENANCE

For valves with double bearing covers with no outside lever of air closing cylinder, preventive maintenance is minimal. The gasket for the bearing covers should be checked for leaks periodically. Also during any period of shutdown, the disc and body seat should be checked for foreign particles, nicks or wear. This may be done by removing the bonnet.

PRESSURE SEAL RING PRECAUTIONS

Due to the customary elapsed time between final shop testing and initial site pressurizing, it is possible for the pressure seal to relax somewhat. We recommend, therefore, that prior to any line filling or pressurizing, the cover nuts be again tightly secured. This assures that the seal ring is firmly in position, ready for pressurizing. The more pressure, the tighter the seal. In other words, some showing of water through the seal with little or no pressure on the valve is not cause for concern as a good application of pressure will generally seal the cover tightly.

GENERAL MAINTENANCE

At valve disassembly, clean and inspect all parts, reworking the parts or replacing them from spare stock as inspection indicates. At reassembly, always use new gaskets.

Before disassembly, always clean and blow down with air any outside surface possible. Any paint or foreign matter such as dirt, rust or scale can greatly hamper the smooth operation of the valve.

Inspection or repair of valve internals can be accomplished without removal of the main valve body from the line.

After surface cleaning and inspection of the valve in the line, disassemble the valve, wire brush all parts and wash them with an approved cleaning solvent, wipe the surfaces with lint-free cloth, or allow the parts to air dry.

Inspect each part carefully for defective threads, excessive wear on seating surface, and bent or worn shaft. Replace any parts found excessively worn or damaged.

## Disassembly - FFRCV With Bolted Bonnet

1. Clean cover area thoroughly.
2. Remove valve cover.
3. Block disc in seating position in valve body.
4. Remove both valve bearing covers from valve sliding them off the dowel pins and shaft.
5. Slide valve shaft out of valve from either side of body.
6. Remove valve disc from valve.
7. Inspect the valve shaft for wear or score marks. If shaft is worn or scored and cannot be repaired it should be replaced.
8. Inspect the seating surfaces of the body and the disc to determine if they require lapping. Any scratches or pitting from foreign matter would be cause for relapping.
9. Use an aluminum lapping plate. Fasten seat width pieces of #180 "grit cloth" to the lapping plate face by means of double backed tape. Leave a small space between the tapes.
10. Block the disc in a flat position, seat up, and lap with a disc lapping plate, either with an air tool or by hand, depending on the amount of lapping required. Lap until scratches and any indentations are removed. Clean grit cloth occasionally by blowing out with air and replace if worn down by prolonged lapping. To check the disc seat, cover with spray-on 603, brush-on-blue or equal. Allow to dry. Lap lightly with seat tool. The seat will be true and polished when all the blue wipes off.
11. Using a body seat lapping plate, lap the body seat using the same procedure as for lapping the disc.
12. After completing the lapping operation, thoroughly clean all parts with acetone or other approved solvent.

Reassembly - FFRCV With Bolted Bonnet

1. Install bushings in bearing covers and into disc arm.
2. Place valve disc in valve body and block it in seating position.

NOTE: Caution should be used to prevent scratching the disc or body seats.

3. Slide shaft through the valve body and disc arm.
4. Install bearing covers to valve body being careful not to damage the dowel pins. Use new gaskets.
5. The seating of the valve can be checked by lifting the disc just enough to insert a  $\frac{1}{4}$ " wide strip of toilet tissue between the disc body seats allowing the disc to seat. This should be checked at four points 90° apart. If at any point the tissue pulls out, the disc is being prevented from seating either from insufficient or improper lapping or a change of seat height from excessive lapping. The chances of the latter happening are extremely remote, but if this is the case, dowel pins should be removed and the bearing cover adjusted until the disc seats firmly all around. Wedge disc firmly in place on its seat and redowel.
6. Make sure after reassembly that bearing covers are in proper alignment and that there is no binding of shaft. Before access cover is replaced, check the end clearances between the disc arm and the bushings to make sure they do not bind on the ends of the disc arm.
7. Clean cover gasket area and install cover gasket and cover.

Disassembly - FFRCV With Pressure Seal Bonnet

1. Clean cover area thoroughly. Remove the four cover nuts.
2. Remove locking plate.
3. If cover does not drop to body shoulder, tap down using a piece of 4" x 4" wood or other suitable means. Again make sure that cover is clean.
4. Remove master segment of load keys. The master segment has parallel ends.
5. Remove balance of load keys.
6. Remove backing ring and again clean area thoroughly as any foreign matter will damage the seal ring and body sealing area during removal of the seal ring.
7. Install eight 3/8" long - all thread steel rods (not supplied) into seal ring tapped holes.
8. It can be useful to use, sparingly, some light approved lubricant around the seal ring to assure smooth removal. Once again it is of the utmost importance to keep the seal ring area clean.
9. Place the locking plate on the body so that the eight 3/8" rods pass through the 1/2" holes in the locking plate.
10. The locking plate is now resting evenly on top of the body face with the 3/8" rods evenly in the 1/2" holes.
11. Lubricate the 3/8" threads.
12. Install eight 3/8" steel hex nuts with 3/8" washers on the 3/8" rods lubricating under the nut and washer faces.
13. Tighten the 3/8" nuts using the diametrically opposed method.
14. The removal of the seal ring will now commence.
15. Once the seal ring is moving easily it may be possible to use four diametrically opposed 3/8" nuts rather than the eight used to start the seal ring moving.
16. The seal ring can now be easily removed using caution when the top of the seal ring enters the area above the load key slot.
17. The body bore area is larger above the load key slot. Care should be taken not to cock the seal ring so that it binds going through this area.

18. The seal ring can now be carefully lifted from the body taking care not to cock the seal ring so that it binds.
19. The cover can now be carefully lifted from the body using a chain hoist.
20. Fasten one end of a sling to the upper section of the disc arm and fasten the other end of the sling to a suitable chain hoist. Take up on the chain hoist so there is just enough tension to support the weight of the disc and arm.
21. Remove the bearing cover nuts and remove the bearing cover. Be careful not to damage the dowel pins when removing the cover. One bushing will remain with the bearing cover. The other bushing will be removed with the shaft.
22. The shaft may be removed from either side of the body. One bushing will be removed with the shaft in the same direction that the shaft is removed. The other bushing can easily be removed after the shaft has been removed.
23. Remove shaft from either side of the body.
24. By means of the sling and chain hoist, lift the disc from the valve through the top cover opening.
25. Inspect the seating surfaces of the body and the disc to determine if they require lapping. Any scratches or pitting from foreign matter would be cause for relapping. If the valve seating surfaces require relapping, hand lap as follows:
26. Use an aluminum lapping plate, these are not furnished with the valve but are available as tools.  
  
Fasten 3" long seat width pieces of #180 "grit cloth" to the lapping plate face by means of double backed tape. Leave spaces of approximately 1" between tapes.
27. Block the disc in a flat position, seat up, and lap with an air tool or by hand, depending on the amount of lapping required. Using a disc lapping plate, lap until scratches and indentations are removed. Clean grit cloth occasionally by blowing out with air and replace if worn down by prolonged lapping. To check the disc seat, cover with spray-on 603 brush-on-blue or equal. Allow to dry. Lap lightly with seat tool. The seat will be true and polished when all the blue wipes off.
28. Using a body lapping plate, lap the body seat using the same procedure as for lapping the disc in Step #27.
29. After completing the lapping operation, thoroughly clean all parts with acetone or other approved solvent.



Reassembly - FFRCV With Pressure Seal Bonnet

1. Insert bushing into disc arm and using sling and chain hoist lower disc into body.
2. Slide shaft through body and disc arm.
3. Insert bushings into bearing cover making sure that they seat on their shoulders.
4. Install bearing cover and dowel to body.
5. The seating of the valve can be checked by lifting the disc just enough to insert a 4" wide strip of toilet tissue between the disc body seats allowing the disc to seat. This should be checked at four points 90° apart. If at any point the tissue pulls out, the disc is being prevented from seating either from insufficient or improper lapping or a change of seat height from excessive lapping. The chances of the latter happening are extremely remote but if this is the case, dowel pins should be removed and the bearing cover adjusted until the disc seats firmly all around. Wedge disc firmly in place on its seat and redowel.
6. Make sure after reassembly that bearing covers are in proper alignment and that there is no binding of shaft. Before access cover is replaced, check the end clearances between the disc arm and the bushings to make sure they do not bind on the ends of the disc arm.
7. Before reinstalling the cover and seal ring all parts should be cleaned and washed with an approved solvent such as acetone.
8. Assure that the seal ring and the stainless steel body sealing area have no nicks or marks that will prevent proper sealing. Dress up with light emery or crocus cloth if necessary.
9. Place cover in body resting on body shoulder.
10. Install seal ring over cover. Again be sure that the cover is absolutely clean. There is a possibility that the seal ring has moved slightly out of round. Therefore, we would suggest locating the best fitting position as the seal ring is starting to enter the body bore. The seal ring should now move down quite easily requiring at most a light tapping to move it into position just below the backing ring area.
11. Place backing ring into position on top of the seal ring.
12. Install segmented load keys.
13. Place locking plate over cover studs and install four hex nuts.

14. Tighten hex nuts using diametrically opposed method evenly and draw cover up evenly being sure it does not strike the load keys and stop there.
15. The cover will now have pulled the seal ring into a sealing position and the hex nuts should be tightened up snugly.
16. When the valve is pressurized, the seal ring will be further forced into position and will seal tightly. The more pressure the tighter the seal. After the cover is sealed tightly with line pressure still in the valve, the hex cover nuts should again be tightened so that the seal will not relax after the valve is depressurized.



STANDARD  
MANUFACTURING PROCEDURE

PAGE

~~3 of 4~~

PROCEDURE NO

90-71-030

Rev. 0

TABLE 1  
BOLT TORQUE (FT. LBS.)

Bolt Size	Bolt Stress (psi)				
	5,000	10,000	15,000	20,000	25,000
1/4-20	1	1	2	2	3
5/16-18	1	2	3	5	6
3/8-16	2	4	6	8	10
7/16-14	3	6	10	13	16
1/2-13	5	10	15	20	25
9/16-12	7	14	21	28	35
5/8-11	10	20	30	40	50
3/4-10	18	35	53	71	89
7/8-9	28	57	85	114	142
1"-8	42	85	127	170	212

ATTENTION: PAT SONTI EXT 85-7752  
 714-368-7654  
 714-368-385  
 FOR A2M NO 15487

714-368-385

85-7752



STANDARD  
MANUFACTURING PROCEDURE

PAGE

~~4 of 4~~

PROCEDURE NO

90-71-03C

Rev. 0

TABLE 2  
ALLOWABLE BOLT STRESS

<u>Bolt Material</u>	<u>Allowable Stress (psi)</u>
A/SA 193-B7	25,000
A/SA 193-B6	20,000 (Note 1)
A/SA 193-B6	21,200 (Note 2)
A/SA 193-B8	15,000 (Note 1)
A/SA 193-B8	18,700 (Note 2)
A/SA 193-B8M	15,000 (Note 1)
A/SA 193-B8M	18,700 (Note 2)
B/SB 150-CDA 630	12,500 (Note 3)
B/SB 150-CDA 630	25,000 (Note 4)

Note 1. Valves built up to 1977 Edition of Code, No Addenda.

Note 2. Valves built to 1977 Edition W/Summer 1977 Addenda or later.

Note 3. Valves built to 1977 Edition up to Summer 1977 Addenda.

Note 4. Valves built to 1977 Edition W/Winter 1978 Addenda or later.

ATTACHMENT 3

MCC-PACIFIC OPERATION AND MAINTENANCE MANUAL

FAMILIAN INDUSTRIAL SUPPLY CO.

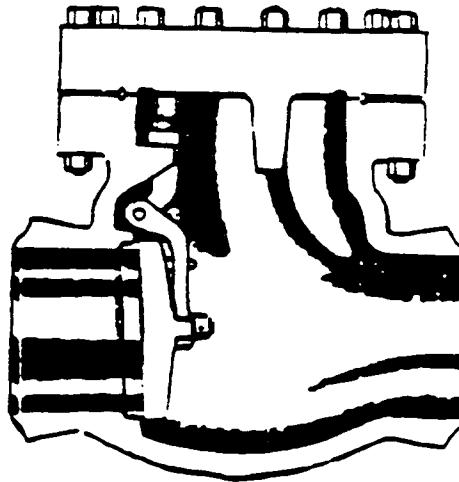
918 Mahar Avenue  
Wilmington, CA 90744

P.O. No. IN 81536

OPERATION AND MAINTENANCE MANUAL

Pacific Valves Shop Job 4L0065

PACIFIC SWING CHECK VALVES



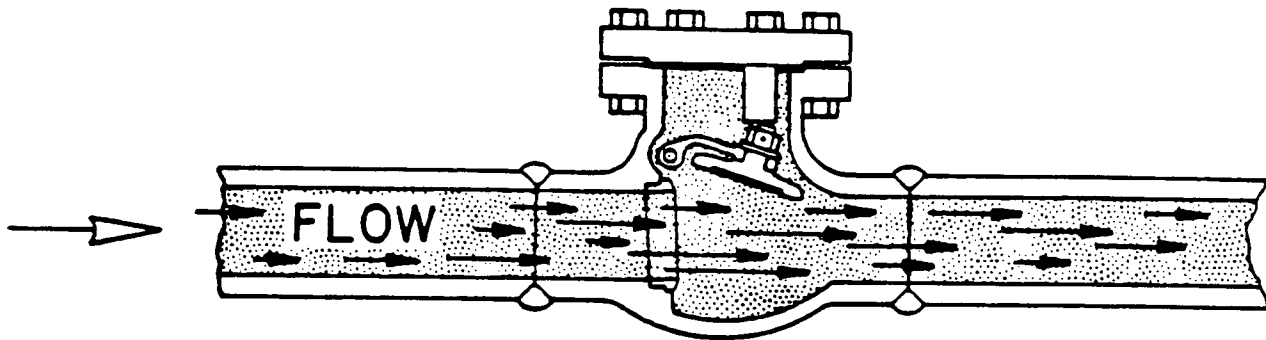
## CONTENTS

- 1.0                    **THEORY OF OPERATION**
  
- 2.0                    **DESCRIPTION**
  
- 3.0                    **INSTALLATION**
  
- 4.0                    **OPERATING INSTRUCTIONS**
  
- 5.0                    **MAINTENANCE**
  
- 6.0                    **PREVENTIVE MAINTENANCE  
(TROUBLE SHOOTING)**
  
- 7.0                    **SPECIAL TOOLS AND INSTRUCTIONS**

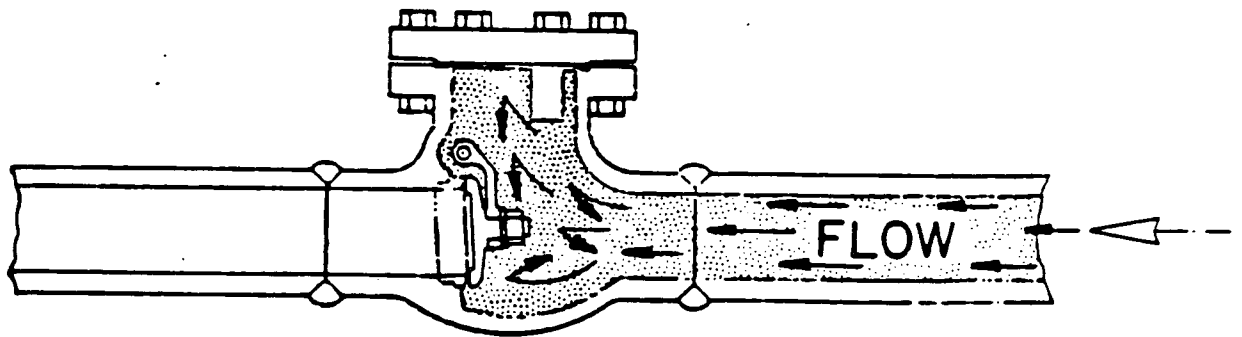


1.0 THEORY OF OPERATION

Swing check valves are designed to open by the pressure of the line. The desired direction of flow in the line will open the valve and any attempt by the flow to reverse will, in its self, close the valve completely. (See illustration below).



DESIRED DIRECTION OF FLOW



REVERSE IN FLOW

THESE DRAWINGS SHOW-GENERAL ARRANGEMENT ONLY.

## **2.0 DESCRIPTION**

This manual covers all Pacific swing check valves. These valves are designed within the limits of ANSI B16.34. Being self-operating, no electrical power, signals or other remote controls or indicators are required. See Section 4.0 for operation of valve.

## **3.0 INSTALLATION**

When unpacking, care should be exercised in lifting and handling to avoid damage to valves or injury to personnel. These valves may be installed in lines varying in angle from horizontal to vertical, provided that the flow is upward. Valves with outside lever and weight are recommended to be mounted only in a horizontal position.

When installing, be certain that all foreign material is removed from the interior of the valve, including desiccants.

A protective paint has been applied to the weld ends on some valves and it should be removed before welding.

For soft seated valves, the temperature of the valve body should not exceed 200°F during welding to avoid damaging the elastomers. Check temperature with Tempil-Stik. Avoid heating valve body excessively, especially small sizes, where a heat sink may be necessary.

Use the smallest electrode and minimum amperage practicable, consistent with efficient welding to minimize warpage.

Tack welds should be ground out before completing the root pass in that area.

Valves of carbon steel should be allowed to cool slowly.

The valve may be covered with an asbestos blanket to promote slow cooling and limit the heat-affected zone.

#### 4.0 OPERATING INSTRUCTIONS

Swing check valves are designed to be operated by the line pressure.

When the line is pressurized, the flow will open the disc.

While the pressure is off or there is back pressure, the disc will be closed.

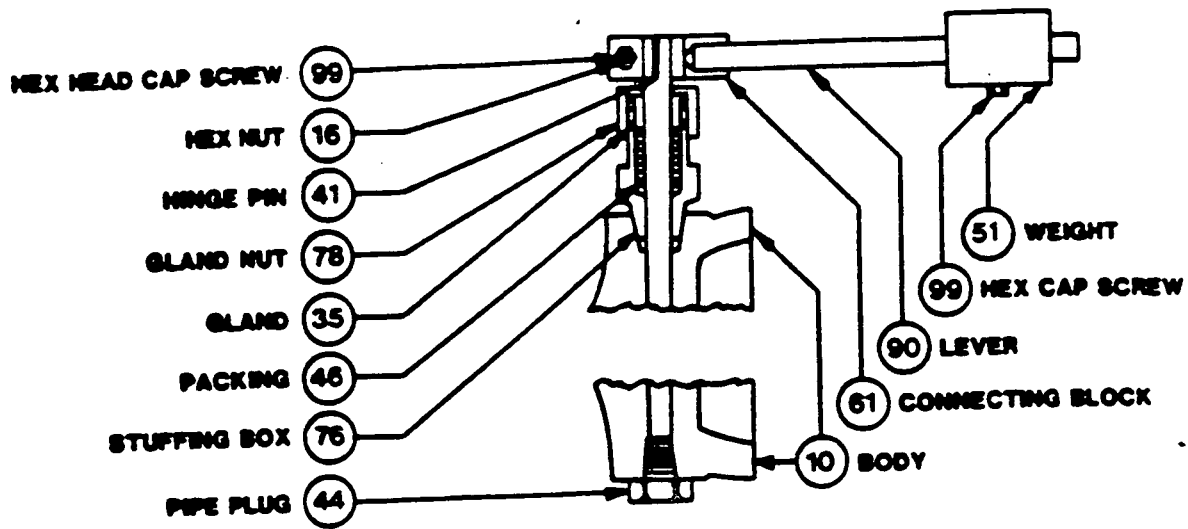
(See illustration in Section 1.0).

#### CAUTION!

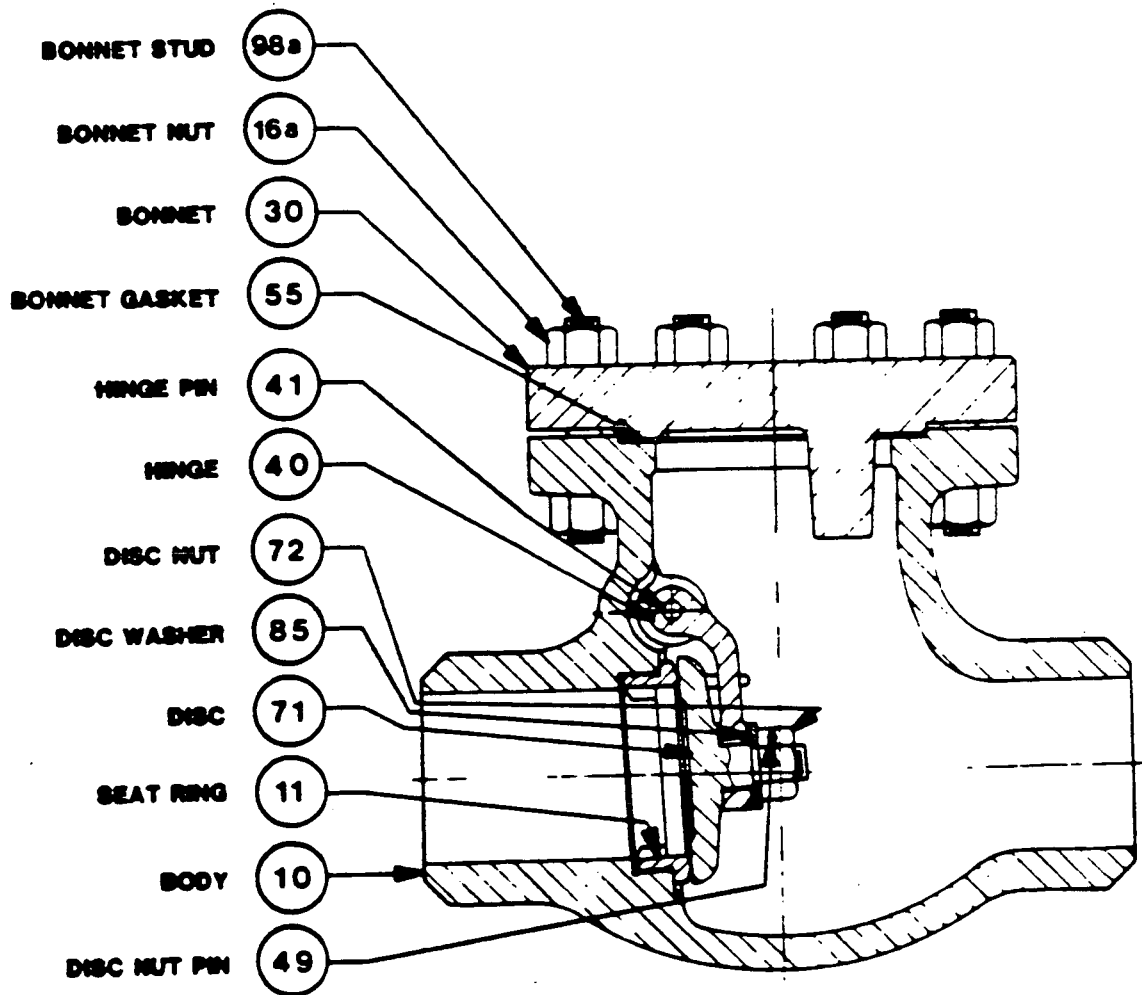
These valves are designed to operate within the pressure and temperature limits of ANSI B16.34. Do not exceed these limits.

#### 5.0 MAINTENANCE

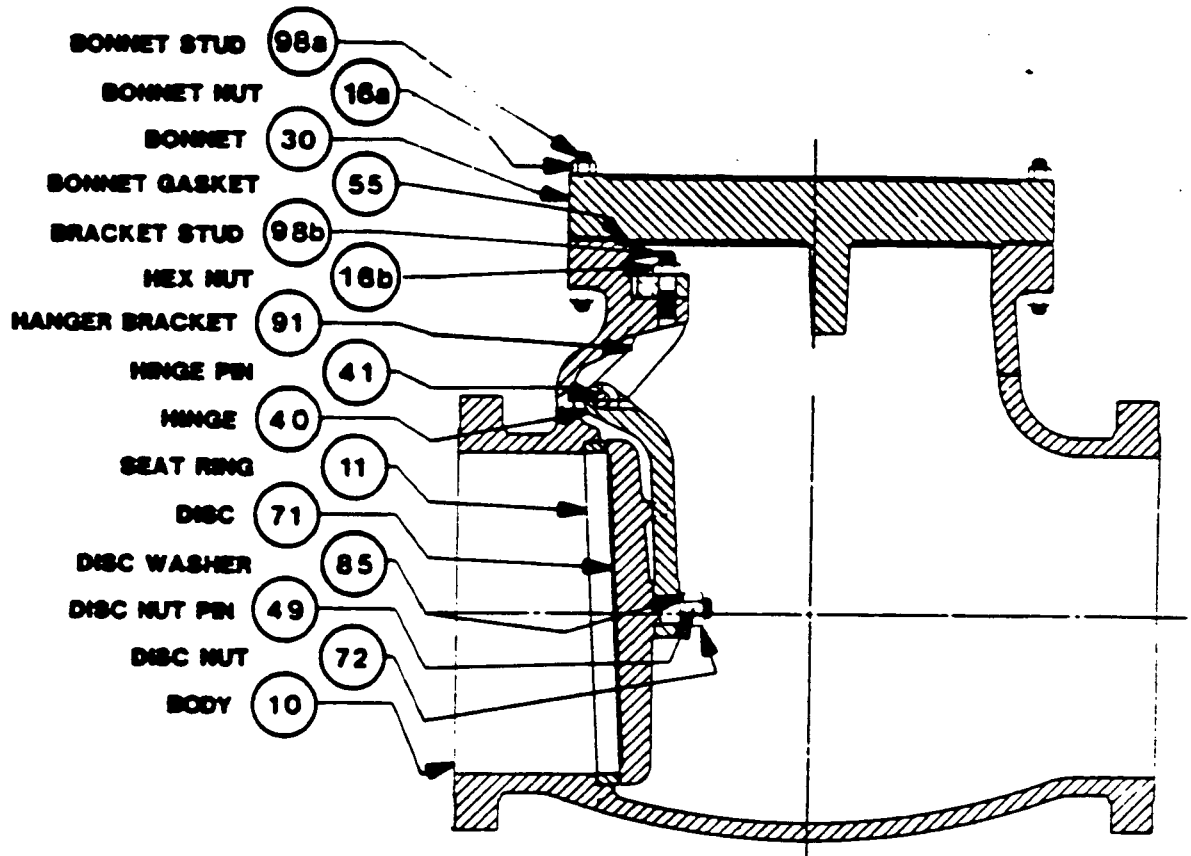
##### 5.1 Complete Disassembly



**SPECIAL OUTSIDE LEVER & WEIGHT ASSEMBLY**



**WELD END SWING CHECK VALVE**



**FLANGE END SWING CHECK VALVE  
 WITH INTERNAL HANGER**

**CAUTION!** Before complete disassembly, make sure no residual pressure is left in the line.

5.1.1 Remove bonnet stud nuts or cap screws (16a) (98a) .

NOTE! Studs need not be removed unless replacement is necessary.

5.1.2 Lift off bonnet cap (30) .

5.1.3 Remove bonnet gasket (55) .

For check valves with internal hanger:

5.1.4 Remove bracket stud nut (16b) . Note: Stud (98b) need not be removed unless replacement is necessary.

For check valves with hinge pin through body:

Remove pipe plugs (44) from both side of body and slip out hinge pin (41) . If pipe plugs are seal welded, they need to be ground free first.

For check valves with outside lever and weight:

Remove connecting block (61) and lever-weight assembly (90) - (99) - (51) .

Remove gland nut (48) and gland (35) .

Remove packing (46) from stuffing box (76)

then remove stuffing box. Remove pipe plug (44) and slip out hinge pin (41) .

5.1.5 Lift out disc assembly (40), (71), (85), (49) and (72) .

5.1.6 Slip out hinge pin (41) . Remove bracket (91) from disc assembly.

5.1.7 Drive out disc nut pin (49) and remove nut (72) in a counterclockwise direction. Slip off washer (85) and hinge (40) from disc (71) .

5.1.8 At this time the seat ring (11) may be removed if necessary. It is usually seal welded to the body (10) and must be cut free. It is advisable to leave it in place unless wear prevents further use.

## 5.2 Complete Assembly

Reverse the steps in Section 5.1. NOTE: If disc has anti-rotation lugs, be sure to replace hinge so that it is aligned between them.

## 6.0 PREVENTIVE MAINTENANCE

### 6.1 Normal Duty Inspection

The only in-service check that can be made is to inspect the body/bonnet gasket joint (55) or hinge pin stuffing box (76) for leaks.

### 6.2 Maintenance of Valve Under Pressure

If the inspection of Section 6.1 reveals any trouble, the following is recommended, if necessary.

6.2.1 If leakage develops at the body (10) bonnet (30) joint, the bonnet stud nuts or cap screws (16a) should be tightened uniformly around the circle.

**CAUTION!**

Do not over stress the bolting  
(See torque charts in Appendix)

If leakage continues, the gasket (55)  
should be replaced.

(See disassembly procedure in Section 5.0).

- 6.2.2 If leakage develops at the stuffing box (76)  
the gland nut (78) can be tightened. If  
the packing continues to leak, the packing (46)  
should be replaced during line shutdown  
(see 6.3).

**6.3 Maintenance of Valve Relieved of Pressure**

**CAUTION!**

**Make certain line pressure is zero.**

- 6.3.1 Following disassembly procedures in  
Section 5.1, examine body cavity (10)  
for deposits of foreign material.
- 6.3.2 Examine seating surfaces of seat ring (11)  
and disc (71) for wear.
- 6.3.3 If excessive wear is evident, worn parts  
or, if necessary, entire valve should be  
reconditioned or replaced.
- 6.3.4 Whenever reconditioning a valve, it is always  
good practice to replace gaskets.



6.3.5 Pacific offers complete replacement seal kits and spare parts for reconditioning. When ordering, always state the figure number of the valve and the body material, as well as the quantity desired.

6.3.6 Pacific Valves also offers complete reconditioning services to rework your valve. If you find this necessary, our nationwide network of reconditioning centers will rebuild your valve "like new".

#### 6.4 Lubrication

6.4.1 Parts requiring lubrication are nuts before torquing and both sides of gasket before assembly.

### 7.0 SPECIAL TOOLS AND INSTRUCTIONS

7.1 Recommended bolting torques are shown in the Appendix.

7.2 No special tools are required.

ATTACHMENT 4

TEST PROCEDURE GUIDELINES

## TEST PROCEDURE GUIDELINE FOR CHECK VALVES LEAKAGE RATE TEST

### I. Functional Test for Check Valves FWS-006, FWS-007 and FWS-012 Inside the Containment:

A. Objective: To verify that the check valve back leakage rates are within the allowable limits. Correct deficiencies if required.

#### B. References:

1. P&ID 5178225, Revision 4, Main Steam System
2. P&ID 5178206, Revision 3, Feedwater System

#### C. Prerequisites:

1. Completion of check valve installation.
2. Verify calibration of pressure gauges.
3. Test to be done during Mode V or VI.
4. Isolation valves (FWS-343, FWS-377, FWS-339, AFW-325, FWS-342, FWS-376, FWS-352, AFW-326, FWS-396, FWS-415, FWS-382 and AFW-328) upstream of the check valves are closed.
5. Establish that the feedwater level of the steam generator at the feed ring elevation  $\pm 2'-0"$ .
6. Nitrogen system blanket is established per procedure.

D. Acceptance criteria: Check valves back leakage rate is within 0.48 gallons per minute at 150 psig. This test procedure was written for testing at 150 psig. Alternate test pressures can be used. The acceptance criteria for using the alternate shall follow the equation.

Allowable leak rate at pres. P,  $Q = 0.48 \sqrt{\frac{P}{150}}$  (gpm), see Fig. 2.

The allowable fluctuation in the test pressure is  $\pm 5$  psi or  $\pm 10\%$  whichever is greater. If test pressures less than 150 psig are used, functional testing of the feedwater main and bypass valves must be done at a test pressure of 150 psig (Test II).

#### E. Method

1. Test the check valve one at a time only. Close isolation valves upstream of the check valve.
2. Connect measuring hose at the designated drain connection (see Table 1) upstream of the check valve. Make sure that the highest point of the connected measuring hose has a minimum loop as it is shown in Fig. 1.

3. Open drain valve (FWS-337, FWS-338, FWS-340, FWS-426 and FWS-424) to depressurize the isolated line upstream of the check valve to atmospheric conditions. To confirm that the upstream isolation valves do not leak, monitor and maintain atmospheric reading on the gauges on the main feedwater and auxiliary feedwater pumps.
  4. Using nitrogen, pressurize the steam generator downstream of the check valve (if pressure is not already established). Monitor and maintain steam generator pressure at 150 psig minimum to 165 psig.
  5. At steady state, and using a container of known volume, measure and record the check valve back leakage rate by measuring the time required to accumulate one gallon. Take two measurement test readings for comparison.
  6. After measuring the check valve back leakage rate, close the nitrogen pressurizing line (if not required for other than testing).
  7. Making sure the system is vented, close the drain valves and disconnect the measuring hose.
  8. Open back all the isolation valves that were closed during the test.
- F. Alternate method for functional test of FWS-006, FWS-007 and FWS-012:

Performance of this test is subject to the availability of the auxiliary feedwater pumps as a pressurization source.

1. With a nitrogen blanket established, initiate auxiliary feedwater flow to pressurize the steam generator. When a test pressure has been established, perform the back leak rate test in accordance with E1 through E5 above. As the pressure will decay during the test, the following requirements apply to the test pressure:
  - a. The decay in steam generator pressure shall be no more than 10% of the final pressure.
  - b. For the purpose of determining the allowable leak rate, the final measured steam generator pressure shall be used.

NOTE: The allowable leakage rate shall be determined using the minimum pressure value obtained during the test.

II. Functional Test for Check Valves FWS-345, FWS-346, FWS-398, FWS-379, FWS-378, FWS-417 in the feedwater system.

A. Objective: To verify that the feedwater system check valves back leakage rates are within the allowable limit. Correct deficiencies if required.

B. Reference:

1. P&ID 5178206, Revision 4, Feedwater System.

C. Prerequisites:

1. Completion of check valve installation.

2. Verify calibration of pressure gauges.

3. Isolation valves (FWS-343, MOV-21, FWS-377, FWS-381, FWS-342, MOV-20, FWS-376, FWS-372, FWS-396, MOV-22, FWS-415 and FWS-419) upstream and downstream of the check valves are closed.

4. Test to be done in Mode V or VI.

D. Acceptance criteria: This criteria applies to the combined check valves back leakage rates of the following paired check valves: FWS-345 and FWS-379; FWS-346 and FWS-378 and FWS-398 and FWS-417 leakage shall be less than 0.48 gallons per minute. This procedure is written using test pressures of 150 psig. Other test pressures can be used. The allowable leak rate at other test pressures shall follow the equation

Allowable leak rate at pres. P,  $Q = 0.48 \sqrt{\frac{P}{150}}$  (gpm), see Fig. 2.

If the test pressure used on the downstream check valves (Test I) is less than 150psig, this test shall be performed at 150 psig minimum.

The allowance fluctuation in the test pressure is  $\pm 5$  psi or  $\pm 10\%$  whichever is greater.

E. Method:

1. Test the check valves one at a time only. Close isolation valves upstream and downstream of the check valve.

2. Connect measuring hose at the designated drain or vent connections (see Table 1). Make sure that the highest point of the connected measuring hose has a minimum loop as it is shown in Fig. 1.

3. Open the drain or vent valve where the measuring hose is connected to depressurize the line to atmospheric conditions. To confirm the upstream isolation valves do not leak, monitor and maintain atmospheric reading on the gauges on the main feedwater pumps.

4. Connect the high pressure water supply to the drain or vent connection designated downstream of the check valve (see Table 1). The water supply must meet the requirement of the chemistry flush specification for the feedwater system. Open the drain or vent valve and high pressure water supply valve and pressurize the line. Using the pressure gauge provided in the water supply hose, maintain and monitor the pressure downstream of the check valve at 150 psig minimum to 165 psig.
5. At steady state, and using a container of known volume, measure and record the check valve back leakage rate by measuring the time required to accumulate one gallon. Take two measurement test readings for comparison.
6. After measuring the check valve back leakage rate, close the drain or vent valve where the measuring hose is connected and disconnect the hose.
7. Making sure the system water is vented, close the high pressure water supply valve and close the drain or vent line valve and disconnect the high pressure water supply.
8. Open back all the isolation valves upstream and downstream of the check valve that were closed during the test.

F. Alternate Procedure:

The back leakage rate test for the feedwater system check valves can also be done during Mode III subject to the availability of the auxiliary feedwater pump as a pressurization source. The following procedure would be used.

1. Test and isolate the check valves one at a time only. Close isolation valve upstream of the check valve.
2. Connect measuring hose at the designated drain or vent connections (see Table 1). Make sure that the highest point of the connected measuring hose has minimum loop as it is shown in Fig. 1.
3. Open the drain or vent valve where the measuring hose is connected to depressurize the line to atmospheric conditions. To confirm the upstream isolation valves do not leak, monitor and maintain atmospheric reading on the gauges on the feedwater pumps.
4. Install a temporary test pressure gauge and open the valve of the vent connection upstream of the check valve as indicated in Table 1.
5. Initiate the auxiliary feedwater pump flow to pressurize the line downstream of the check valve to within  $\pm 10\%$  of the normal operating pressure. Maintain and monitor the pressure at the test pressure gauge installed at the vent connection.

6. At steady state, and using a container of known volume, measure and record the check valve back leakage rate by measuring the time required to accumulate one gallon. Take two measurement test readings for comparison.
7. After measuring the check valve back leakage rate, close the drain or vent valve where the measuring hose is connected and disconnect the hose.
8. Close the vent connection valve where the test pressure gauge is installed and remove the gauge.
9. Open back all the isolation valves upstream of the check valve that was closed during the test.

### III. Functional Test for Check Valves FWS-438 and FWS-439 in the feedwater system.

- A. Objective: To verify that the feedwater system check valves are still intact and functional.

Correct deficiencies if required. These valves have been provided with a 9/32" orifice hole drilled in the check valve disc. Standard leak rate tests cannot be performed. This testing will determine the functionality of the check valve.

B. Reference:

1. P&ID 5178205, Revision 2, Feedwater System.

C. Prerequisites:

1. Completion of check valve installation.
2. Verify calibration of pressure gauges.
3. Isolation valves (FWS-441, FWS-469, CV-875B, HV-854B, FWS-556, FWS-440, FWS-472 and HV-854A) upstream and downstream of the check valves are closed.
4. Test to be done during Mode V or VI.

- D. Acceptance criteria: When the downstream piping is pressurized to 150 psig the upstream leakage rate is less than 20 gpm. Other test pressures can be used. The allowable leakage rate at an alternate pressure P would follow the equation

$$Q = 20 \sqrt{\frac{P}{150}} \quad (\text{GPM})$$

The allowable fluctuation in test pressure is  $\pm 5$ psi or  $\pm 10\%$  whichever is greater.

E. Method:

1. Test the check valve one at a time only. Close isolation valves upstream and downstream of the check valve.
2. Connect measuring hose at the designated drain or vent connections (see Table 1). Make sure that the highest point of the connected measuring hose has a minimum loop as it is shown in Fig. 1.
3. Open the drain or vent valve where the measuring hose is connected to depressurize the line to atmospheric conditions. To confirm the upstream isolation valves do not leak, monitor and maintain atmospheric reading on the gauges on the main feedwater pumps.



4. Connect the high pressure water supply to the drain or vent connection designated downstream of the check valve (see Table 1). The water supply must meet the requirement of the hemistry flush specification for feedwater system and can provide 20 gpm at 150 psig minimum pressure to 165 psig. Open the drain or vent valve and high pressure water supply valve and pressurize the line. Using the pressure gauge provided in the water supply hose, maintain and monitor the pressure downstream of the check valve at 150 psig minimum to 165 psig.
5. At steady state and using a container of known volume, measure and record the check valve back leakage rate by measuring the time required to accumulate ten gallons. Take two measurement test readings for comparison.
6. After testing, close the vent valve where the measuring hose is connected and disconnect the hose.
7. Making sure the system is vented, close the high pressure water supply valve and close the vent line valve and disconnect the high pressure water supply.
8. Open back all the isolation valves upstream and downstream of the check valves that were closed during the test.

F. Alternate Method for Functional Test of FSW-438, FWS-439.

This method is subject to the availability of the feedwater pumps as a pressurization source during mode 5 or 6. Test only one check valve at a time feedwater system will be aligned such that, one feedwater pump will be run and the water will be recirculated to the condenser via the 3" miniflow line. The check valve on the discharge of the out-of-service feedwater pump will be tested as follows;

1. Establish feedwater flow and flow path from one feedwater pump close the upstream isolation valve on the check value on the discharge of tag out-of-service pump.
2. With the flow path in the crosstie between the feedwater heaters open, install a temporary pressure gauge on the pressurized side of the check value.
3. Connect measuring hose at the designated drain or vent connections (see Table 1). Make sure that the highest point of the connected measuring hose has a minimum loop as it is shown in Figure 1
4. Open the drain or vent valve where the measuring hose is connected to depressurize the line to atmospheric conditions.
5. At steady state, and using a container of known volume, measure and record the check valve leakage rate by measuring the time required to accumulate 20-40 gallons.

6. After measuring the check valve back leakage rate, close the drain or vent valve where the measuring hose is connected and disconnect the hose.
7. Making sure the system is vented, terminate Feedwater miniflow.

**CAUTION:** Care should be taken when performing this alternate testing, as the potential exists for overpressurization of the feed water suction piping. The suggested test pressure is 150 psig.

IV. Functional Test for Check Valves AFW-321, AFW-322, AFW-324, in the Auxiliary Feedwater Systems. (Continued)

B. Reference: P&ID 5178220, Revision 5 Auxiliary Feedwater System.

C. Prerequisites:

1. Completion of check valve installation.
2. Verify calibration of pressure gauges.
3. Isolation valves( AFW-325, FCV-2300, AFW-326, FCV-3301, FCV-2301, AFW-338, FCV-3300,) upstream and downstream of the check valve are closed.
4. Test to be during Mode V or VI.

D. Acceptance criteria: Check valve back leakage rate is within 0.48 gallons per minute. This procedure is written using test pressures of 150 psig. Other test pressures can be used. The allowable leak rate at other test pressures shall follow the equation.

Allowable leak rate at pres. P,  $Q = 0.48 \sqrt{\frac{P}{150}}$  (gpm), see Fig. 2.

The allowable fluctuations in test pressure is  $\pm 5$ psi or  $\pm 10\%$  whichever is greater.

E. Method:

1. Test check valve one at a time only. Close isolation valves upstream and downstream of the check valve.
2. Connect measuring hose at the designated connections upstream of the check valve (see Table 1). Make sure that the highest point of the connected measuring hose has a minimum loop as it is shown in Fig. 1 is higher than the highest point of the isolated line where it is connected (see Fig. 1).
3. Open the drain or vent valve where the measuring hose is connected to depressurize the line to atmospheric condition. To confirm the upstream isolation valves do not leak, monitor and maintain atmospheric reading on the gauges on the auxiliary feedwater pumps.
4. Connect the high pressure water supply to drain or vent connection designated downstream of the check valve (see Table 1). The water supply must meet the requirement of the chemistry flush specification for the feedwater system. Open the drain or vent valve and the high pressure water supply valve and pressurize the line. Using the pressure gauge provided in the water supply hose, maintain and monitor pressure downstream of the check valve at 150 psig to 165 psig.

5. At steady state, using a container of known volume, measure and record the check valve back leakage rate by measuring the time required to accumulate one gallon and the check valve minimum downstream pressure value. Take two measurement test readings for comparison.
6. After measuring the check valve back leakage rate, close the valve where the measuring hose is connected and disconnect the hose.
7. Making sure the system is vented, close the high pressure water supply valve and close the vent or drain valve where high pressure water supply is connected and disconnect the high pressure water supply line.
8. Open back all the isolation valves upstream and downstream of the check valve that were closed during the test.

TABLE 1

CHECK VALVE	HIGH PRESSURE SUPPLY CONN.	MEASURING CONNECTION	ISOLATION VALVES
FWS-006		FWS-338	FWS-376, AFW-326, FWS-352 and FWS-342
FWS-007		FWS-337	FWS-339, FWS-377, FWS-343 and AFW-325
FWS-012		FWS-424	FWS-382, FWS-396, FWS-415 and AFW-328
FWS-417	FWS-432	FWS-423	FWS-415 and FWS-419
FWS-398	FWS-368	FWS-365	FWS-396 and MOV-22
FWS-378	FWS-428	FWS-422	FWS-376 and FWS-372
FWS-346	FWS-446	FWS-366	FWS-342 and MOV-20
FWS-379	FWS-423	FWS-421	FWS-377 and FWS-381
FWS-345	FWS-425	FWS-367	FWS-343 and MOV-21
FWS-439	FWS-445	FWS-565	HV-854B, HV-852B, CV-875B and FWS-473
FWS-438	FWS-540	FWS-510	FWS-440, FWS-556, FWS-472 and HV-854A
AFW-321	DRAIN	VENT	AFW-325 and FCV-2300
AFW-322	DRAIN	VENT	AFW-326, FCV-3301 and FCV-2301

(2002k)

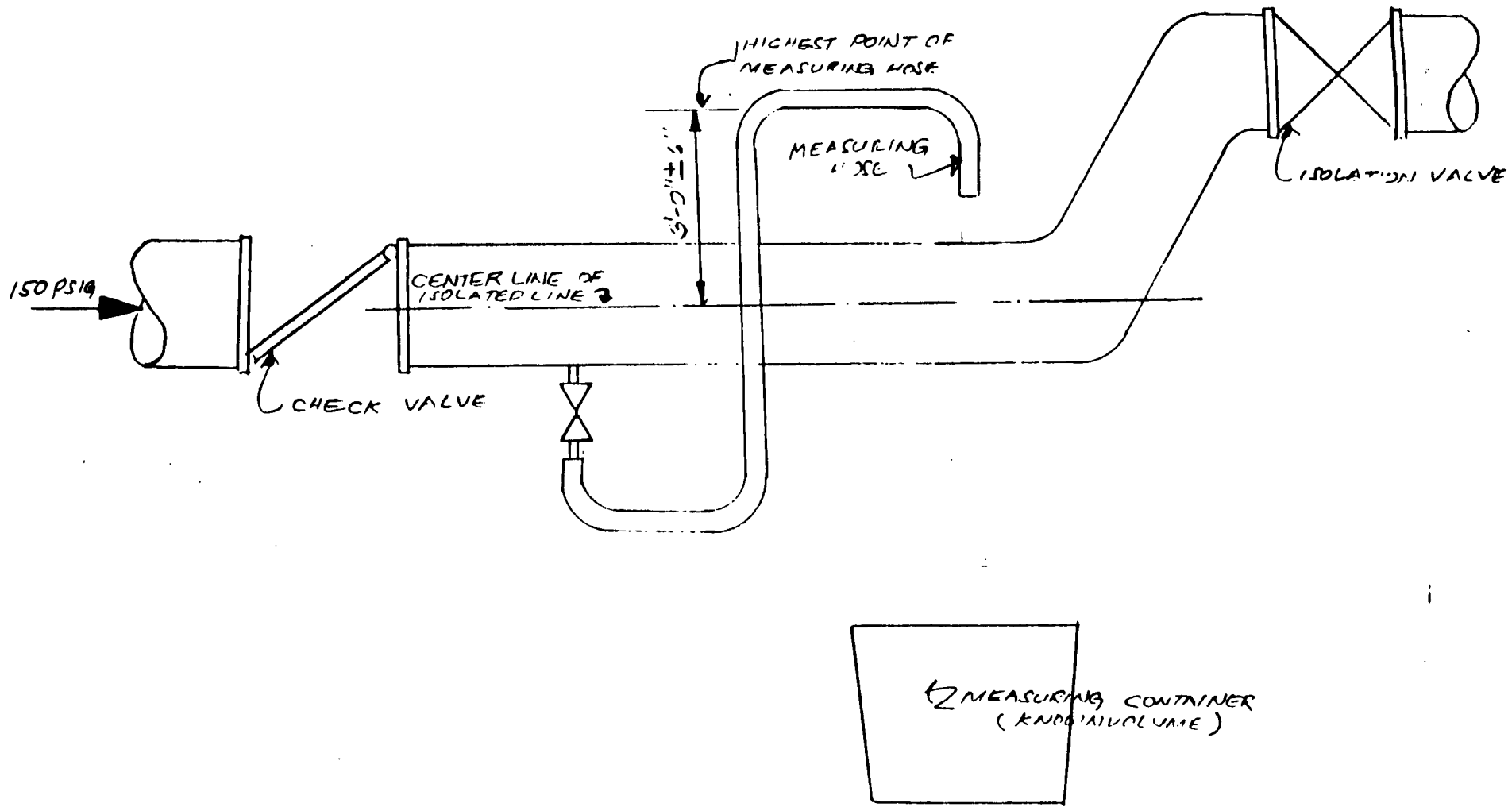
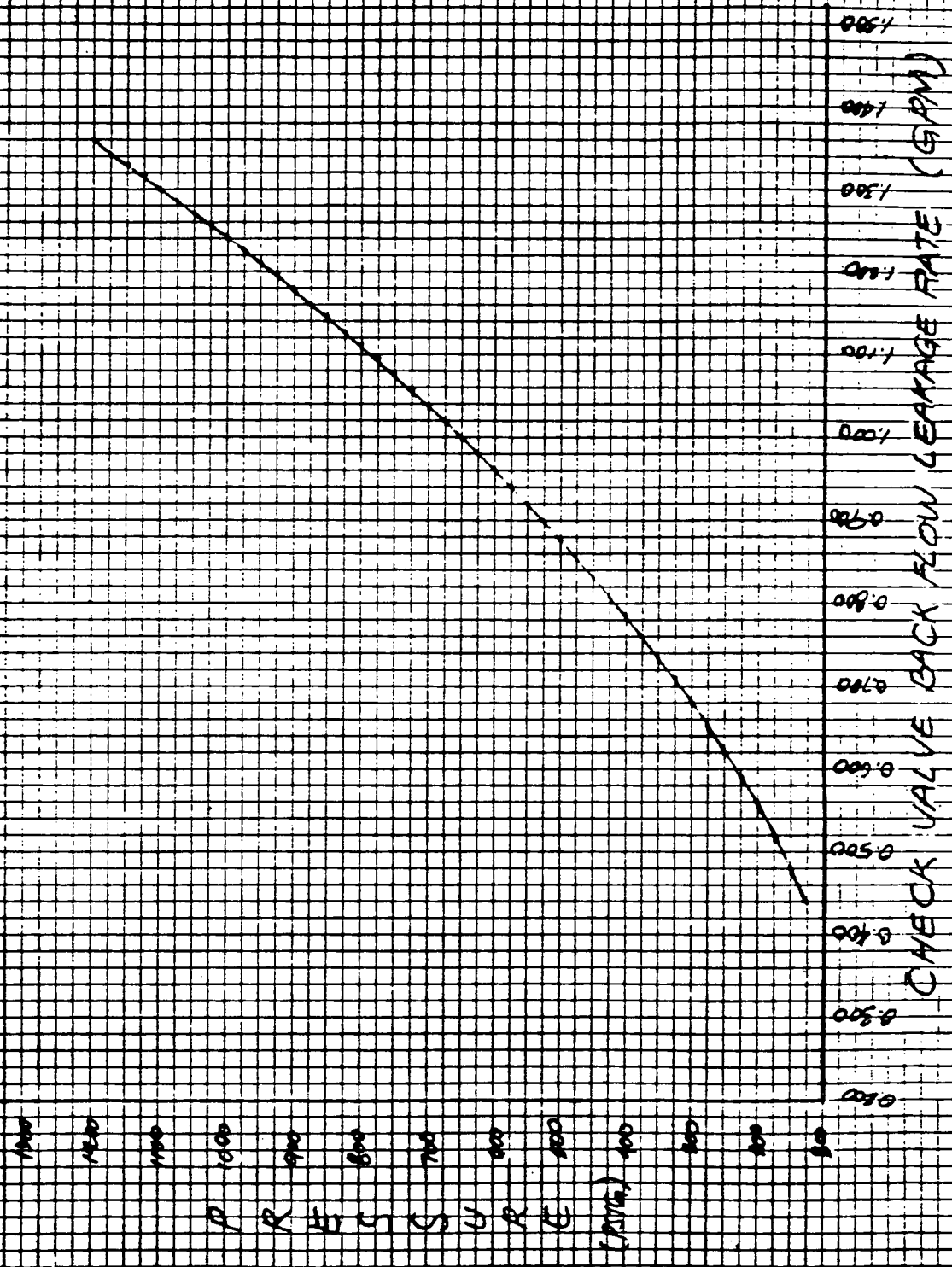


FIG. 1 - TYPICAL HOSE AND MEASURING HOSE FOR CHECK VALVE BACKFLOW LEAKAGE TEST.

FIG. 2 - ALLOWABLE CHECK VALVE  
BACK FLOW LEAKAGE RATE



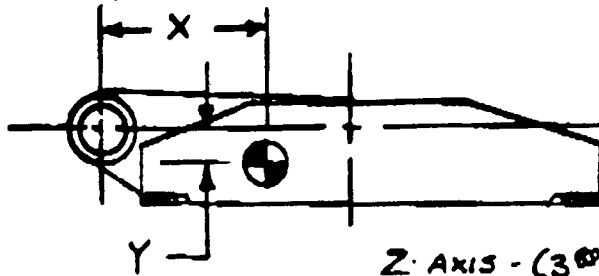
NOTE: TESTS SHOULD BE PERFORMED AT 150PSI9 OR GREATER  
WHENEVER POSSIBLE.

ATTACHMENT 5

CENTER OF GRAVITY SKETCH



DISC WEIGHT / CG -- 900 # DBC BFPCV'S



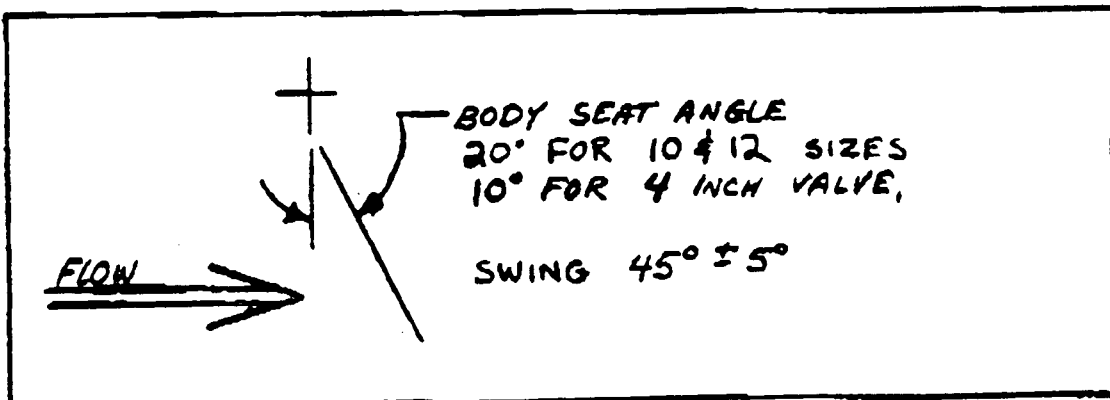
☒ THRU SHAFT HUB.

Z-AXIS - (3<sup>RD</sup> DIMENSION)  
CG IS ON PIPE/VALVE ☒.

TO: RICHARD JENSEN BECHTEL POWER NORWALK CA	FR. E. BOLTON ATWOOD & MORRILL SALEM MA.
---	--

EJB  
4-11-86

SIZE	REF.	WGT	X	Y
10	15487-01 15487-05 15487-06 15487-07	51 LBS.	4.65 IN.	.54 IN.
12	15487-02	86 LBS.	6.03 IN.	.64 IN.
4	15487-03	6.2 LBS.	2.17 IN.	.14 IN.



QUESTION NO. 3

Vibratory Loads

- a. Clarify the method of development of the factor that turbulence loads from upstream components will not exceed 10% of disc weight?
- b. The ISA Handbook of Control Valves provides recommendations on installation. Why or why can't these locational restrictions be correlated to check valves?
- c. Atwood-Morrill recommends not locating check valves within specific distances of turbulence producing components. What is the basis for deviating from these recommendations?

RESPONSE

- a. For the response to this question, reference Appendix D of the SCE Investigation Report submitted to the NRC by letter dated April 8, 1986.
- b. The ISA Handbook, Chapter 12, page 339 (Attachment 1), recommends 10-20 pipe diameters of straight run piping upstream of control valves and 3-5 pipe diameters downstream. The handbook acknowledges that the 10-20 diameters upstream may be next to impossible to obtain in line sizes larger than nominal 5". These values actually correlate quite well with those of 10 pipe diameters upstream and 5 diameters downstream given as optimum by Atwood-Morrill for their check valves. However, as explained in our response to Question 3c, Atwood-Morrill check valves can be located at less than these optimum conditions without experiencing any significant vibration or disc flutter.
- c. Per a February 24, 1986 letter from L. Hutton of Atwood-Morrill (Attachment 2), they do not expect any problems resulting from the chosen check valve locations. Independent tests conducted at Utah State University Foundation by Dr. P. Tullis, demonstrate the acceptability of the Atwood-Morrill valves at all of the San Onofre Unit 1 feedwater check valve design locations. The most severe location is downstream of the flow control valves. This testing confirms the acceptability of locating the check valve five diameters downstream of the control valve.

ATTACHMENT 1

ISA HANDBOOK, PAGE 339

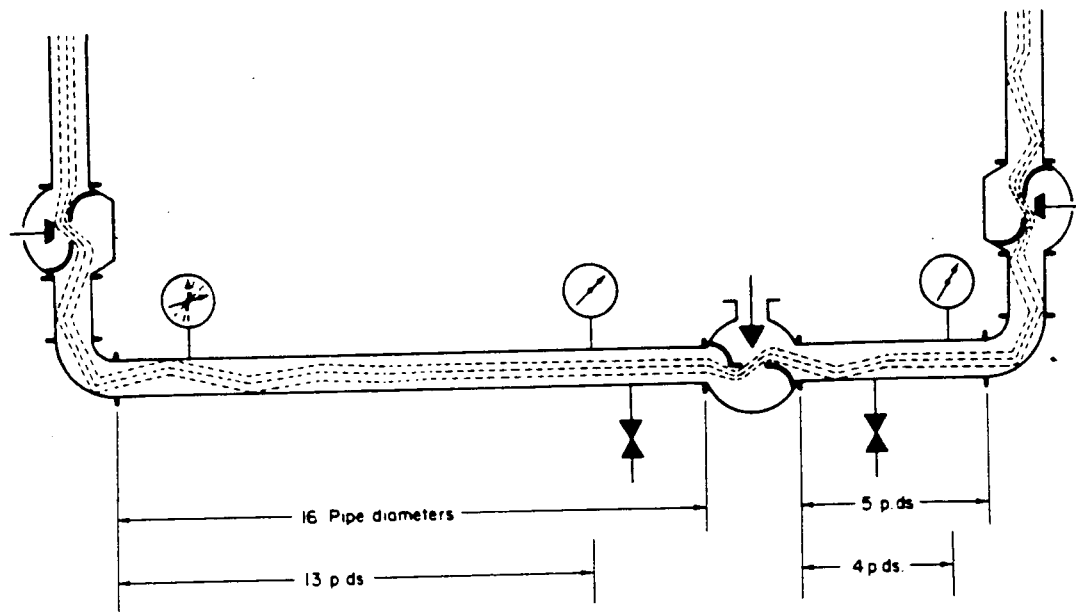


Figure 3. TYPICAL SATISFACTORY ARRANGEMENT OF UPSTREAM AND DOWNSTREAM PIPING.

control engineer's calculations, or vice versa. Figure 2 shows a method of plotting system pressures to arrive at available pressure drop vs. valve lift. A similar plot will be used by the valve manufacturer to accurately design the valve plug. The piping design engineer should review such plots in designing the piping system. The design friction loss, through the lengths of pipes and fittings selected, can be made consistent with such plots. This calculation should include the friction drop through the fully opened control valve as part of the piping system. The characteristic pump curve is generally available from the pump manufacturer. The terminal pressure drop vs. flow through the process vessel may be more difficult to obtain.

It can be seen from Figure 2 that valve performance—capacity and flow vs. valve lift, will be altered if the actual piping system consumes more pressure drop (curve 4) than that considered in the valve sizing calculation.

In designing the inlet and exit piping at a control valve, a conservative approach is to consider the control valve as a variable orifice; thus, the piping recommendations used to pipe orifice plate assemblies can be applied. The following considerations are recommended:

1. Allow the maximum number of feet of straight run inlet piping that is consistent with other piping demands. A good rule of thumb is 10 to 20 pipe diameters. This is easy to obtain in small size lines,

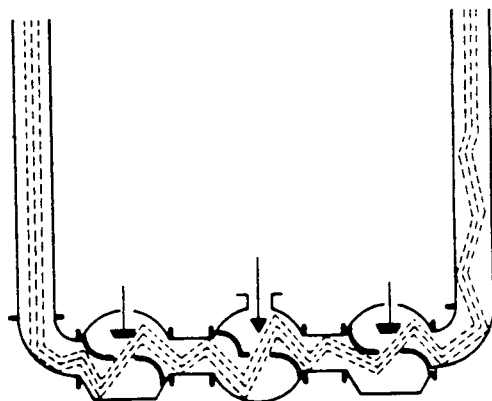


Figure 4. A LESS SATISFACTORY ARRANGEMENT OF UPSTREAM AND DOWNSTREAM PIPING.

but may be impossible to obtain in line sizes larger than nominal 5 inches. Nonetheless the practice of allowing for a maximum straight inlet run will allow better valve performance.

2. Where possible, allow a straight run of 3 to 5 pipe diameters for the outlet piping.
3. The straight run on the inlet to the valve will permit the fluid stream to enter the valve at a steady inlet pressure. Thus, for every position taken by the valve, or in other words, for every new orifice opening, a steady inlet pressure condi-

ATTACHMENT 2

ATWOOD-MORRILL LETTER DATED 02/24/86

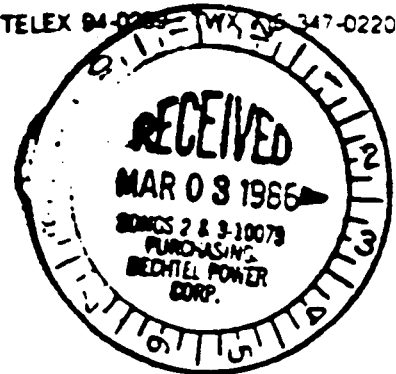


**ATWOOD & MORRILL CO. INC.**  
DESIGNERS AND MANUFACTURERS SINCE 1900

PRVB36-6208

285 CANAL STREET · SALEM MASSACHUSETTS 01970 · 617 744-5690 · TELEX 94-0285 · FAX 617-347-0220

February 24, 1986



Bechtel Power Corporation  
Post Office Box 60860  
Terminal Annex  
Los Angeles, CA 90060

Attention: Mr. Fred Lizmi

Subject: Your P.O. No. VB200603  
Southern California Edison  
Feedwater Check Valves  
A&M S.O. No. 15487

Reference: Your February 14, 1986 letter transmitting  
pipe configuration and valves location dwgs.

Gentlemen:

While it is true that during the meeting with representatives of Bechtel and Southern California Edison, I recommended that no piping changes be made prior to installing our valves, we cannot guarantee that you will never encounter problems. However, based on our past experience with this design which includes approximately 30 years installed operating experience in similar applications with no major failure, we are confident that the valves will perform as specified for a full design life of 40 years. It is because of this successful operating experience that we felt that Southern California Edison should avoid the expense of reconfiguration of their piping systems. During the meeting, I noted that if problems did occur, the piping could then be modified.

The optimum installation location for check valves would include 10 pipe diameters upstream and 5 pipe diameters downstream of straight piping without other valving or reducers. Although this is optimum, in the real world of power plant design this configuration cannot always be adhered to. We note many similar Atwood & Morrill valves installed immediately after an elbow, in between two elbows, and even close coupled to a pump discharge with an elbow immediately downstream of the valve, again with no major failure.

Some of the reasons for the successful operation history of this design are as follows:

- 1) The 20° seat angle minimizes impact velocity due to a lower disc swing angle between full open and full closed.
- 2) The integral disc/disc arm assembly cannot separate as is typical with the conventional two piece disc assemblies in swing check valves.
- 3) The substantial disc stop restricts disc opening angle assuring that the disc cannot become jammed open and that the disc is in the flow stream and be forced to close upon flow reversal.

Should you have any further questions concerning this or require further clarification, please do not hesitate to contact us.

Very truly yours,

ATWOOD & MORRILL CO., INC.

*Lauren Hutton*

Lauren C. Hutton  
Vice President Sales

LCH/ko  
LCH 22

Enclosure

c: Robert Burns & Associates, Inc.

Mike Macdonald - A&M

QUESTION NO. 4

What was the procurement history for the original valves and spare parts?

RESPONSE

The original valves were procured under Bechtel Specification BAL-560, a portion of which appears in the Attachment. Due to the age of the microfilm for which the copy was made, the quality of the print is poor but is the best available.

As discussed in Section 6.5.3.4 of the Water Hammer Investigation Report, there was some difficulty in retrieving maintenance records for the failed check valves. The efforts to date have been unsuccessful in locating spare parts procurement records and additional efforts are not planned.



BECHTEL SPECIFICATION BAL-560

ALAMITOS STEAM STATION, UNITS NO. 5 AND 6

CAST STEEL, CAST IRON AND BRONZE VALVES

SPECIFICATION NO. MAL-560

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ATTACHMENT A - Electric Motor Operated Gate and Globe Valves

ATTACHMENT B - Limit Switches on Manually Operated Gate and Globe Valves



1.01 DEFINITIONS (Continued)

A. "Specification" - The Instructions and Information to Bidders, Special Conditions, Drawing and Data Requirements, the Specific Conditions, the Proposal Bidding Sheet, and any Supplement, Drawings, Schedules and data sheets attached thereto, or reference herein, together with the Conditions of the Purchase Order, comprise the complete specifications.

B. "Purchaser" - The Bechtel Corporation.

C. "Owner" - The party or parties on whose behalf the Bechtel Corporation acts as Engineer, Contractor and/or Construction Manager.

D. "Vendor" - The party or parties negotiating contracts with the Purchaser for the work specified herein.

E. "Bidder" - The party or parties submitting proposals for the work.

F. "Work" - All work specified in the Specifications, including the furnishing of all labor, plant, materials, equipment, services and all other items necessary, and the performance of all other work specified in the Specifications and the work specified.

When "as shown," "as detailed," "as indicated," or words of like import are used, it shall be understood that reference to the project drawings is made unless stated otherwise. Where "as directed," "as required," "as approved," "Acceptance," or words of like import are used, it shall be understood that the direction, requirement, approval, or acceptance of the Purchaser is intended.

1.02 DRAWINGS The Drawings are the property of the Bechtel Corporation and shall not be used for any other purpose than the instant purpose.

1.05 PROPOSALS

A. Proposals shall be submitted in a drip-proof envelope enclosed in a sealed envelope distinctly marked "Proposal" with the name and address given, and delivered to Bechtel Corporation, Attention: B. A. Bohner, Purchasing Supervisor, 4550 Seville Avenue, Vernon, California, on or before the appointed hour.

B. The proposal shall be signed with the full name and local address of the Bidder; if a co-partnership by a member of the firm with the name and address by each member; if a corporation, by an officer, in the corporate name, and with the corporate seal.

C. Unless otherwise stipulated herein, the Purchaser reserves the right to reject any and all proposals, to accept other than the

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2.05 PROPOSALS (Continued)

lowest proposal, to accept or reject the same, or to combine proposals, or to reject any proposal, or to request technical information from any proposal.

2.1. The specifications for the items to be purchased shall be as set forth in the invitation of a revised proposal with the exception that the specifications of the proposals will be the basis for the award.

2.2. The specifications for the items to be purchased shall be as set forth in the invitation of a revised proposal with the exception that the specifications of the proposals will be the basis for the award.

2.3. STANDARD PRODUCTS Except for standard products which are normally manufactured and available in the United States, the intention of the purchaser is to purchase the items specified herein. The items specified herein are the items which are regularly used by the purchaser and are the items which are specified in the invitation of a revised proposal. The purchaser's intent is to purchase the items specified herein as an alternative.

2.4. ACCEPTANCE OF PURCHASE ORDER  
The purchaser shall promptly execute an order for the items specified herein. The order shall be in accordance with the terms and conditions of the invitation of a revised proposal. The order shall be in accordance with the terms and conditions of the invitation of a revised proposal. The order shall be in accordance with the terms and conditions of the invitation of a revised proposal. The order shall be in accordance with the terms and conditions of the invitation of a revised proposal.

341-10 (6)

BECHTEL CORPORATION

Vernon, California

SPECIAL CONDITIONS

(Vendor)

308 4666

2.01. STANDARD OF DESIGN AND WORKMANSHIP

A. The finished work shall be complete in all respects and shall fully conform to the description there set forth in the contract order.

B. The intent of the specifications is to secure for the Purchaser work of first class workmanship in all respects. All components shall be manufactured, fabricated, assembled and finished with workmanship of the highest quality throughout, and in accord with the best of recognized correct practice. All materials shall be of the quality and to the conditions specified.

2.02. INSPECTION, TEST AND EXPERIMENT The Owner and the Purchaser and either alone, shall be allowed access to the Vendor's shops and those of the Vendor's suppliers to inspect and or experiment the work and workmanship and to obtain other desired information. The Vendor shall furnish to the Owner and the Purchaser, if so requested, at an additional cost, shop and mill test reports when specified. The Vendor shall inform the Purchaser of progress of the work and shall give the Purchaser ample advance notice of appropriate times for inspection and test. Specified tests will be approved and supervised by the Purchaser. When specific inspections or tests are required, the work involved shall not proceed beyond that point until the Purchaser has made or waived such inspections or tests.

2.03. ACCEPTANCE The acceptance of the work will be given after the Purchaser has made sufficient tests and inspections to determine the compliance of the work with the specifications and any written agreements between the Vendor and the Purchaser. Tests and inspections will be made within six (6) months from the date work is complete and ready for use. If tests and/or inspections show the work not to be as represented or contracted for, the Purchaser may refuse to accept it and the Vendor shall be so advised, and given a reasonable time to make the necessary corrections. All corrections shall be made at the Vendor's expense.

2.04. WARRANTY

A. Vendor shall warrant that all materials, labor, work and all parts thereof to be furnished and performed hereunder shall be of the kind

BALELO 01



2.04 WARRANTY (Continued)

and quality as described in the Specific Conditions shall be guaranteed for the use contemplated and shall perform in the manner specified therein and no other warranty by the Vendor or such suppliers, except of title, shall be implied. Vendor obligations under this warranty extend to both Purchaser and Owner for enforcement by either Purchaser or Owner or both.

B. Should any non-compliance, defect or failure to fulfill such warranty appear within one year from date of "Turbine Roll", Vendor shall correct the defective work, or defective designs, as the case may be, by repairing the defective part or parts, by correcting the design, or by supplying a non-defective replacement thereof without delay and at its expense to the Purchaser or Owner. Such repair, correction or replacement shall constitute complete fulfillment of the obligation of Vendor under this warranty, and upon expiration of the applicable warranty period specified therein, all such obligations shall terminate, except as provided in Paragraph (C) hereof.

C. In the event that Vendor or their suppliers, as the case may be, shall correct any defective parts or work pursuant to Subparagraph (A) or (B) hereof, then with respect to the parts or work corrected, the above said warranty period shall run for one (1) year from the completion of such correction.

2.05 CHANGES: The Purchaser shall have the right to make reasonable changes at any time in drawings and specifications by a Change Order in writing. In the event any such change is ordered and such change causes an increase or decrease in the amount due and/or in the time required for performance, an equitable adjustment of the price and/or time of performance shall be made in accordance therewith.

2.06 FORCE MAJEURE:

A. Vendor shall not be held responsible or liable for any loss, damage, detention or delay caused by fire or strike, civil or military authority or insurrection or riot, or by any other cause which is beyond his reasonable control.

B. Vendor and its suppliers shall not be liable to the Owner or Purchaser for any consequential damages resulting from the performance or nonperformance of the work included herein.

2.07 RIGHT TO USE WORK REQUIRING CORRECTION: After installation, the Purchaser and/or Owner shall have the right to use work which may require correction by the Vendor until such time as it is convenient to the Purchaser that this work be removed from service for correction.

2.08 SHIPMENT, DELIVERY AND PIECE MARKING: The work shall be shipped in assembled units, insofar as is consistent with good shipping practice. When items must be dis-assembled for shipment they shall be match-marked. All

BAL 10/61



2.08 SHIPMENT, DELIVERY AND RISK OF LOSS

units and their containers shall be clearly marked with the purchase order number. Machines and their important parts shall be protected from impact and weather damage with all necessary padding.

2.09 TITLE: The title to the work herein specified shall remain in the vendor until the vendor delivers the work in the manner for repairs to the purchaser. This provision shall not be construed to require the purchaser to repair or inspect the work so delivered, and to reject any portion thereof if repairs were provided.

2.10 INSURANCE: In order to permit the purchaser to insure the work delivered to the purchaser, the vendor shall be responsible for obtaining and maintaining sufficient insurance to cover the work. The vendor agrees to advise the purchaser, in writing, of the date of each shipment, giving detailed information as to the contents, weight, and of the value of each such shipment and to enable the purchaser to obtain and maintain such insurance.

2.11 TAXES: The purchaser agrees to pay any and all applicable taxes or use taxes imposed by Federal, State, County, or other governmental authority, by any foreign government and the sales tax liability, where the purchaser remains the vendor for all such taxes required to be paid and actually paid by the vendor, except that the purchaser shall not be held liable for any and shall promptly be reimbursed by the vendor if it ever pays any amount of amounts of sales or use taxes levied or assessed against the vendor or the purchaser by reason of any failure of the vendor to comply with the provisions of Section 211 of the California Constitution or any other statute thereof or of other provisions of the California State Tax Code, or if it is alleged by applicable taxing authorities to result in the passage of title to the work at a point other than is specified in the Purchase Order. In which case Special Conditions are a part. If the delivery point specified in the Purchase Order is outside the State of California and the vendor is authorized to collect California use tax, the vendor shall show his California State Use Tax Permit Number on all invoices.

2.12 SEGREGATION OF FREIGHT CHARGES: Freight charges, if the vendor elects to prepay the same, shall be stated separately in invoices applicable thereto.

10/10/61

**3.01 PURPOSE.** This Specification states the requirements for the furnishing and delivering of valves for the Station. The station will be of the Station. Universal Pressure Bolts supplying Station.

**3.02 CONDITIONS OF AWARD.** The Bidder shall submit his bid and shall be liable to his general catalog and shall indicate the quantity and extent of firm price. It is contemplated that a quantity of valves of the type specified will be selected on the basis of proposals received and a blanket award issued to the Bidder submitting the most attractive offer. Requests for shipment will be issued as engineering and construction progress. These "requests" will list specific quantities, sizes, grades, etc. and will constitute authorization to make shipment as indicated.

**3.03 BID REQUIREMENTS:** Bids are required in the following categories:

A. Cast carbon or chrome-nickel steel gate valves, 1/2 inch and larger, 150 psi through 300 psi.

B. Cast iron gate, globe and check valves, 1/2 inch and larger, 125 psi and 250 psi.

C. Bronze gate, globe and check valves, 1/2 inch and larger, 125 psi through 200 psi.

**3.04 GENERAL REQUIREMENTS**

A. Code. Casting, fittings, etc. shall conform to the applicable ASTM or ASA Standards. Pressure and temperature ratings shall also conform to designated codes.

B. Finish. All seating and sliding surfaces shall be properly finished to prevent seizing, galling, spalling, chipping or other undesirable conditions that may hinder normal operation of the valves or prevent shut-off during normal usage.

C. Drawing and Data requirements (To be Furnished by the Supplier).

Type of Drawing or other Information Required	No. Copies Required Each Drawing
1. Outline Dimensions (If not in Vendor's regular catalog)	None
	After Award (Within 15 Days)

3.04 GENERAL REQUIREMENTS (Continued)

Type of Drawing  
or other  
Information Required

Program (Insert ID Box)

\* 2. Motor Operated Valve

- A. Wiring Diagrams
- B. Catalog Information
- C. Orientation of Motor  
on Valve

Note  
None  
None  
None

3. Installation Instructions  
and Parts List

None  
None

\*Wiring Diagrams and motor operator orientation drawings shall be submitted to the Purchaser for approval before the Motor Operator process and valve fabrication. Drawings submitted for approval shall be returned to the Vendor within 15 days with our comments or approval.

B. The equipment provided under this specification shall comply with the latest requirements of the Southern California Edison Company for this class of material.

3.05 TESTS

A. Hydrostatic Tests. Valves shall be checked for sand, slag, chips or other foreign matter before hydrostatic testing is made.

B. The Vendor shall conduct all tests required by ASTM Specification and shall keep a complete record. Castings from any heat not meeting the specification requirements shall be rejected. All valves shall successfully pass hydrostatic shop tests as to body and seat tightness in accordance with Vendor's standard practice.

The Purchaser's Inspector may be present at any of the tests, and, if he so requests, shall be furnished with two certified copies of the results, whether or not he is present at the actual test.

3.06 DEFECTS: Defects which do not impair the strength of the casting may be repaired by an approved process. The defects shall be cleared out to solid metal before repairing. All steel for forgings and castings shall be heat treated after welding in accordance with requirements of the ASTM Code. Valve bodies and welding shall be properly heat treated and stress relieved. (Cast Steel Valves only).

**3.07 MARK NUMBERS:** The designated mark number shall be applied to a weather-proof metal tag securely fastened to each valve by either spot welding or riveting.

**3.08 SURFACE PREPARATION AND PAINTING (Cast Steel and Iron Valves Only)**

A. Exterior ferrous surfaces to be protected by painting shall be cleaned in accordance with the "Steel Structure Painting Manual, Surface Preparation Specifications No. 6 Commercial Blast Cleaning." The surface profile of the blast pattern shall not exceed 2 mils.

B. After completion of all tests and inspection, all unfinished exterior surfaces of each valve will be painted with one coat of paint conforming to Federal Specification No. TT-66A, Type II.

**3.09 SHIPPING PREPARATION:** Finished beveled ends shall be suitably protected by covering other than oils, grease or paint as protection against damage during transit or storage. Other finished surfaces shall be adequately protected against damage. Unpainted ferrous metal other than machine beveled ends may be covered with grease before shipment. The valves shall be closed by plugs or covers securely fastened before shipment.

**3.10 LOCAL FACILITIES:** Each bidder shall include a complete description of his local service facilities, including his ability to install new cast rings in valves in service at the jobsite, availability of personnel for field service, policy and procedure for rectifying quality operation and material.

**3.11 EXPOSURE**

A. Indoors. - relative humidity up to 85 percent.

B. Outdoors. - Subject to the corrosive conditions of fog, salt spray and dust, relative humidity of 100 percent and air temperatures varying from approximately 40F to 100F.

**3.12 DELIVERY:** Prices shall be furnished to cover the period between April 1, 1964 and April 1, 1966.

**NOTE TO BIDDER:** It is considered that book list prices include special paint and packing on all cast steel valves and special paint on cast iron valves. Preferential discounts applicable to book list prices may be adjusted accordingly, if necessary.

## SPECIFIC REQUIREMENTS - ASME TYPE VALVES

4.01 DESIGN: Gate and globe valves shall be made with wedge type Gate valves shall have single wedge discs. Globe valves shall have single type plug discs. Check valves shall have wing type discs. Valves shall have stainless steel seat rings and 12 percent chromium plug or disc. Stainless steel overlay of disc or plug surfaces for pressure-retaining parts shall be used.

Bonnet joints on all valves shall be flanged and bolted to provide ready accessibility to the valve internals. Seat rings for all gate valves, globe valves and check valves shall be renewable and shall be either screwed or pressed in place and fully seat welded.

Castings on all carbon steel valves shall conform to ASTM Specification A-216 Gr. WCB. Chrome - Moly valves shall be cast in accordance with ASTM Specification A-217.

4.02 PACKING: Gate and globe valves shall be provided with stem packing, molded to fit the gland and suitable both for the service application and hydrostatic tests. Gate and globe valves shall have button gland packing and shall be back-sealed so the valve stem can be packed even if the valve is open and in service. All valves shall be packed with Grade 304 stainless steel packing.

4.03 CONNECTIONS: No Bypass Valves are to be furnished on any valve. Valves requiring by-passes or drains shall have a long schedule or capped nipple welded in locations indicated on the purchase order.

### 4.04 END SEPARATIONS

A. Flanged valves shall have standard ASA flanges and serrated flanges on each end with standard bolting and face to face dimensions corresponding to pressure-temperature rating of the valve.

B. Butt weld end valves shall have standard ASA bevel on each end and shall be bevel to match standard or extra strong pipe size as indicated on "Request to Ship" form.

4.05 ELECTRIC VALVE OPERATORS: Electric motor operated valves shall be furnished in accordance with attached Motor Operated Valve Specification. (Attachment A).

4.06 LIMIT SWITCHES: Limit switches, when required on manually operated valves, shall be furnished and mounted in accordance with the attached Specification for Limit Switches. (Attachment B).

4.07 GEAR OPERATORS: When required, gear operators shall be Bevel type with either open or enclosed gearing. The pinion shaft shall be extended and shall terminate in a machined 7/8" hexagon end to suit the socket of an air operated wrench.

4 US AIR WRENCHES FOR VALVE OPERATION: Approximately 200 lbs. Power  
Tool Co. Reversible Nut Setters, Fig. No. 57X-225 (RSM), with 7/8 inch  
sockets and 25 foot piece of 1/2 inch 100-psi air hose with 1/2 inch  
coupling and No. 2180 nipple will be required.

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812-560

SPECIFIC REQUIREMENTS - CAST IRON VALVES

5.01 DESIGN: Gate and globe valves shall be iron and shall have a rising stem, outside screw, bolted flanged gate-body. The gate shall be a solid disc with end flanges faced and drilled according to ASA Standard B16.1. Valves shall be bolted cap with renewable bronze seat and stem type disc. All bodies, bonnets and caps are to be cast iron and shall conform to ASME A-12b, Class 2.

SPECIFIC REQUIREMENTS - BRONZE VALVE

6.01 DESIGN: Gate, Globe, Lift and Swing Valves will be rated for 125 ps steam at 353F through 200 ps steam at 538F pressure class. Gated or flanged. Gate and Globe Valves shall be inside screw union bonnet type stem, dictator bronze alloy renewable or pressed in seat ring or integral seat with same material with solid hardened alloy renewable disc.

Both Horizontal Lift Type and Swing Check Valves, stems or handles, will be required in 150 and 200 pound steam ratings. All body bonnet and cover assemblies shall conform to ASTM B61 Specification.



QUESTION NO. 5

Were other types of valve designs considered for this application (e.g., tilting or damped disk)? What is the basis for choosing a swing check design?

RESPONSE

In considering other types of valve designs, the primary focus was on the tilting disc type due to its short arc of travel. The geometry of the Atwood-Morrill swinging disc is such that the arc of travel from full open to full close is very similar to that of a tilting disc but without the detriment of having the disk and hinge suspended in the flow path. Atwood-Morrill, in fact, does not make a tilting disc check valve but instead offers the subject swing check valve as its equivalent.

The original Westinghouse valve equipment Spec. 675268, paragraph 4.2.3, dated 12/16/64 (Attached), also recommended swing type check valve for valves 2" and larger.

The damped disc was not considered for this application as this type of valve would not mitigate any of the check valve problems experienced on San Onofre Unit 1.

WESTINGHOUSE VALVE E-SPEC 675268, page 6

**EQUIPMENT SPECIFICATION COVER SHEET**  
WESTINGHOUSE FORM 54064 A

114  
E Spec.  
675268

EQUIPMENT SPECIFICATION 675268	DATE 12/16/64	REVISION NO. 0	DATED	ORIGINAL ISSUE <input checked="" type="checkbox"/>	SUPERSEDES PREVIOUS REVISIONS <input type="checkbox"/>
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**ATTACHMENTS**

- Ⓢ Drawing 498 B 932
- Ⓢ APD E.D. SK. 322694
- Ⓢ PS 292722-1  
Specification Sheets

**PROJECT:** SAN ONOFRE NUCLEAR GENERATING STATION, UNIT NO. 1

**SHOP ORDER:** SCE-220

**SYSTEM:** ALL SYSTEMS

**EQUIPMENT:** MANUAL GLOBE, MANUAL GATE, AND SELF-ACTUATED CHECK VALVES

**FOR SUPPLIER'S CONVENIENCE**

REV. NO.	REVISION ENTERED BY & DATE

WESTINGHOUSE ELECTRIC CORPORATION  
Atomic Power Division  
P.O. Box 355  
Pittsburgh, Pennsylvania, 15230

**APPROVAL**

	ORIGINAL ISSUE	REV. 1	REV. 2	REV. 3	REV. 4
<b>AUTHOR</b>	<i>J.R. Blanchfield</i>				
<b>SHOP ORDER HOLDER</b>	<i>[Signature]</i> 12/16/64				
<b>PROJECT MANAGER</b>	<i>H. von Holde</i> 12/17/64				

# EQUIPMENT SPECIFICATION

## 4.0 REQUIREMENTS

### 4.1 Service Requirements

- 4.1.1 The design of each valve shall accommodate the design conditions set forth on the valve "Specification Sheet" for the particular valve.
- 4.1.2 All stainless steel valves shall be suitable for service in demineralized water containing up to 12% boric acid ( $H_3BO_3$ ).
- 4.1.3 All carbon steel valves shall be suitable for service in demineralized water inhibited with KOH and  $K_2CrO_4$ .
- 4.1.4 Some of the valves of this specification will be exposed to the step changes of working fluid temperature described below. If these thermal transients are thought to be too severe for the supplier's standard valves, the supplier shall so advise. WAPD will then indicate which valves must be suitable for the thermal transients and review the necessary modifications to the supplier's valves.

The thermal transients are:

- a. 150 cycles of a step change of plus or minus  $300^{\circ}F$  (or a temperature differential equal to the valve design temperature less  $40^{\circ}F$ --whichever is smaller) and
- b. 10 cycles of a step change from  $500^{\circ}F$  (or the valve design temperature--whichever is lower) to  $40^{\circ}F$ .

### 4.2 Mechanical Design Requirements

Any exceptions to the following will be as stated on the "Specification Sheet" for the individual valve.

- 4.2.1 Gate valves may be either straight through or venturi type providing the valve pressure drop is acceptable to WAPD. The wedge may be either split or solid. All gate valves shall have backseat and outside screw and yoke.
- 4.2.2 Globe valves shall be full-ported with backseat and outside screw and yoke.
- 4.2.3 ~~Check valves shall be spring-loaded lift or in-line type for sizes 1/2 inch and smaller and swing type for sizes 2 inches and larger.~~
- 4.2.4 The pressure containing parts of the valve assemblies shall be designed in accordance with ASA B16.5 or in accordance with MSS SP-66.

WESTINGHOUSE ELECTRIC CORPORATION  
ATOMIC POWER DIVISION

WAPD FORM 412

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to E-Spec. <u>675268</u>	

QUESTION NO. 6

What flow band can result in a valve disk flutter problem for each of the new valves?

RESPONSE

Atwood-Morrill has an integral hinge/disc design and as such the disc cannot "flutter" about the hinge arm.

Per testing results reported by P. Tullis, the flowbands which cause disc "tapping" (intermittent contact of the disc assembly with the valve body) -are as follows:

<u>Location</u>	<u>Plant Flow (gpm)</u>
12" Valves Downstream of Feedwater Pumps	3650 - 5700
10" Valves Downstream of Flow Control Valves	2600 - 3900
Proposed 10" Valves Inside Containment	2700 - 3050

In all cases the tapping was not judged to be severe enough to cause damage to the valve body or disc over long term service. Phase 1B testing is planned to develop wear rate information on the valves.

QUESTION NO. 7

Include a discussion on how the auxiliary feedwater operating flow band avoids disk flutter or vibration from other check valves in the main feedwater and auxiliary feedwater piping system.

RESPONSE

The check valves currently installed in the 3" auxiliary feedwater lines were originally sized based on the auxiliary feedwater flow rates. The operating history of the plant indicates that these valves have performed satisfactorily. Therefore, there is no reason to discontinue the use of these valves.

The new 10" Atwood-Morrill valves in the main feed system have been tested at low flowrates representative of the auxiliary feedwater flows and found to be totally stable. Additionally, there was virtually no downstream pressure fluctuations generated by the valve at any flowrate.

QUESTION NO. 8

Clarify the statement made in handouts used at the January 31, 1986 meeting with the NRC that an error existed in Crane Technical Paper 410 that may have contributed to this problem.

RESPONSE

The following statement was provided during the referenced meeting in the course of discussing the cause of the multiple check valve failures:

"Valves were oversized for the range of line flow due to 1965 design - guide error (Crane Technical Paper No. 410); the 1986 Crane design guide as well as the check valve vendor's 1986 design practice identify the failed check valves as oversized (valve will not be fully opened)."

The following information is provided from Appendix D to SCE's report of April 8, 1986.

The equation used by MCC Pacific Valves for the minimum velocity to maintain the check valve disc fully open has changed over the years. These changes are depicted in Table 4 of Appendix D. The 1978 minimum velocity recommended by Pacific was based upon the minimum velocity published by Crane for its swing check valves. In 1982, Crane revised its equation for minimum velocity. These and other changes were much less than what was recommended in a 1985 revision to Pacific's recommended minimum flow velocity.

SCE believes that to have characterized the Crane document as being in error was inappropriate. It appears that the revisions in the equation given by Crane were based upon results of more recent tests. It should merely be noted that application of the revised Pacific recommendation (based upon the 1985 Bulletin on Technical Information) is more appropriate and demonstrates that the Pacific valves are improperly sized for this application.

QUESTION NO. 9

Submit the results of the re-analysis of the auxiliary feedwater (AFW) initiation timing requirements that determine how quickly the emergency diesel generators must be manually loaded in the case of a loss-of-offsite power and a single failure of the turbine-driven AFW pump.

RESPONSE

See the attached reanalysis.



## ENCLOSURE 1

### Loss of Normal Feedwater and Main Feedline Rupture Reanalysis

San Onofre Unit 1

#### BACKGROUND

The Loss of Normal Feedwater (LONF) event and the Main Feedline Rupture (FLB) event were analyzed in 1981<sup>(1)</sup> for Southern California Edison's (SCE) SONGS-1. The analysis concluded that an auxiliary feedwater (AFW) flowrate of 165 gpm, initiating 3 minutes after reactor trip, to 3 steam generators was required to show acceptable results for the LONF (with reactor coolant pumps (RCP) operational) event. An AFW flowrate of 250 gpm, initiating 15 minutes after reactor trip, to 2 steam generators was shown to be needed to provide acceptable results for the FLB (with RCP's operational) event. The LONF and FLB events were reanalyzed to determine if specified maximum delays of operator initiation of the AFW for the LONF and FLB events are acceptable.

The LONF event was reanalyzed assuming loss of RCP's, modelling SONGS 1 specific RCP coastdown, 1979 ANSI Decay Heat, and an AFW flow of 165 gpm to 3 steam generators initiated 30 minutes after reactor trip. The FLB event was reanalyzed with the same loss of RCP's and decay heat assumptions but with a delay of 20 minutes after reactor trip for initiation of an AFW flow of 250 gpm to 2 steam generators.

#### ANALYSIS

As in the 1981 LONF and FLB analysis, the LOFTRAN code (2) is used to simulate the transients. The reanalysis consists of 2 cases. The assumptions modelled in the 2 cases are the same assumptions used in the 1981 analysis except as noted below.

CASE 1: Loss of Normal Feedwater with AFW flow of 165 gpm at 30 minutes.

#### Assumptions:

- A. Loss of reactor coolant pumps with SONGS-1 specific RCP coastdown is modelled. An operating pump heat addition to the RCS of 3 Mwt/pump is assumed.
- B. 1979 ANS 5.1 Decay Heat is modelled.
- C. Pressurizer power-operated relief valves and pressurizer sprays are available.

- D. 20% steam generator tube plugging parameters with plant initially operating at 103 percent of rated power is assumed.
- E. Reactor trip is assumed to occur 10 seconds into the transient. (Same as 1981 analysis)

CASE 2: Feedline Break with AFW flow of 250 gpm at 20 minutes.

Assumptions:

- A. Loss of reactor coolant pumps with SONGS-1 specific RCP coastdown is modelled. An operating pump heat addition to the RCS of 3 Mwt/pump is assumed.
- B. 1979 ANS 5.1 Decay Heat is modelled.
- C. Pressurizer power-operated relief valves are available, but no credit is taken for pressurizer sprays.
- D. 20% steam generator tube plugging parameters with plant initially operating at 103 percent of rated power is assumed.
- E. Reactor trip is assumed to occur 5 seconds into the transient. (Same as 1981 analysis)

## RESULTS

### CASE 1: Loss of Normal Feedwater

The results of the transient of pertinent plant parameters are shown in Figures 1-1 through 1-7. The figures show that the AFW flow of 165 gpm to 3 steam generators initiated 30 minutes after reactor trip provides acceptable results. The assumed AFW flow provides sufficient heat removal capability. A maximum pressurizer water volume of 1139 ft<sup>3</sup> (88% of total pressurizer volume) was obtained at 2553 seconds.

### CASE 2: Feedline Break

The results of the transient are presented in Figures 2-1 through 2-7. The results show that the AFW flow of 250 gpm to 2 steam generators initiated 20 minutes after reactor trip is sufficient to remove core decay heat. The reactor coolant system (RCS) remains subcooled and the pressurizer does not fill, with a peak pressurizer water volume occurring at 1483 seconds.

## CONCLUSIONS

Results of the analysis show that for the LONF with loss of RCP's, an AFW flow of 165 gpm to 3 steam generators initiated 30 minutes after reactor trip provides acceptable results. An AFW flow of 250 gpm to 2 steam generators initiated 20 minutes after reactor trip is adequate to remove decay heat for the FLB with loss of RCP's event.

## LIST OF REFERENCES

1. Letter from K. P. Baskin (SCE) to D. M. Crutchfield (NRC) dated November 18, 1981, Enclosure 1 titled, "Figures 1-10 AFWS Reanalysis San Onofre Unit 1"
2. Burnett, T. W. T., et al., "LOFTRAN Code Description," WCAP-7907-A, April, 1984.

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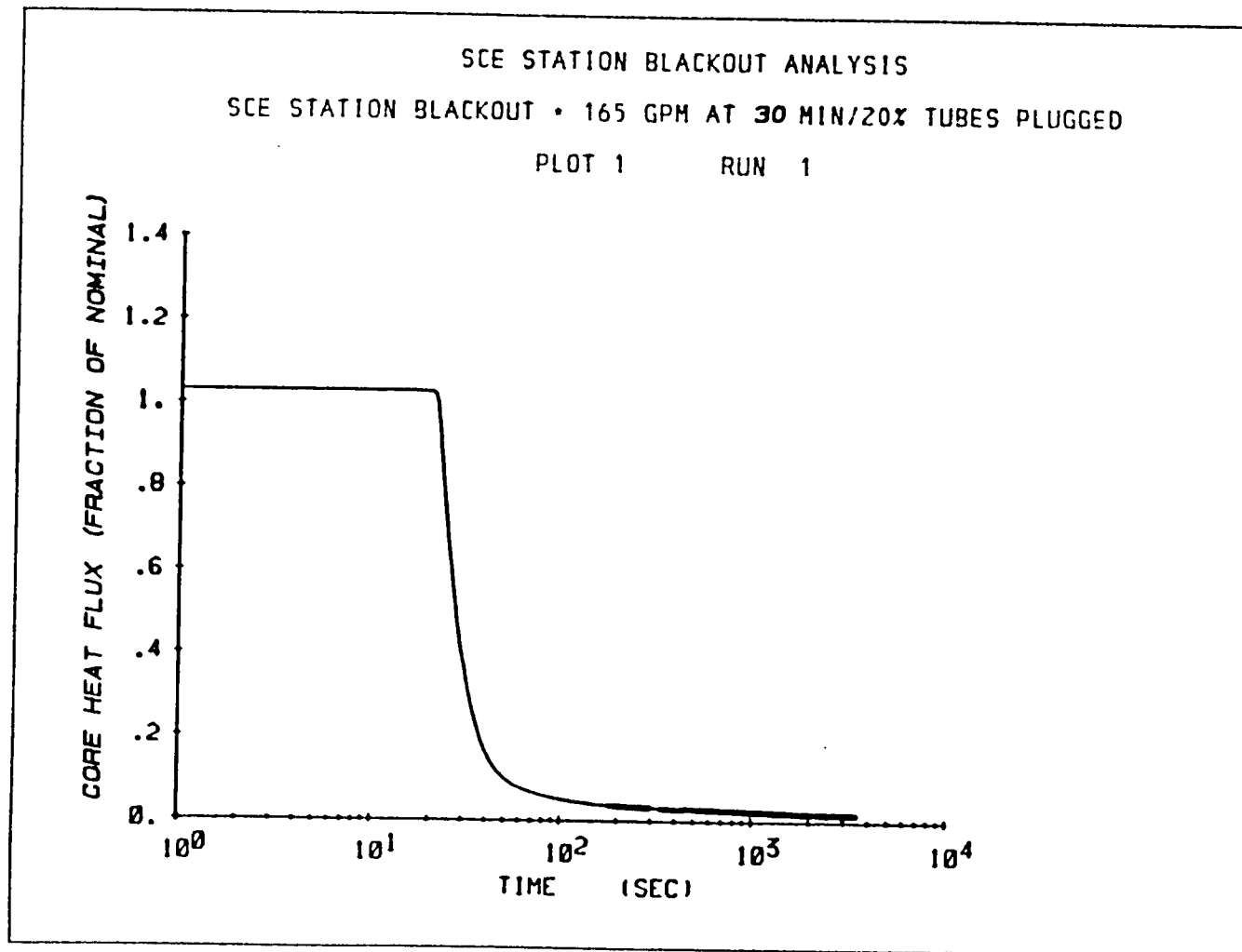


FIGURE 1-1 CORE HEAT FLUX

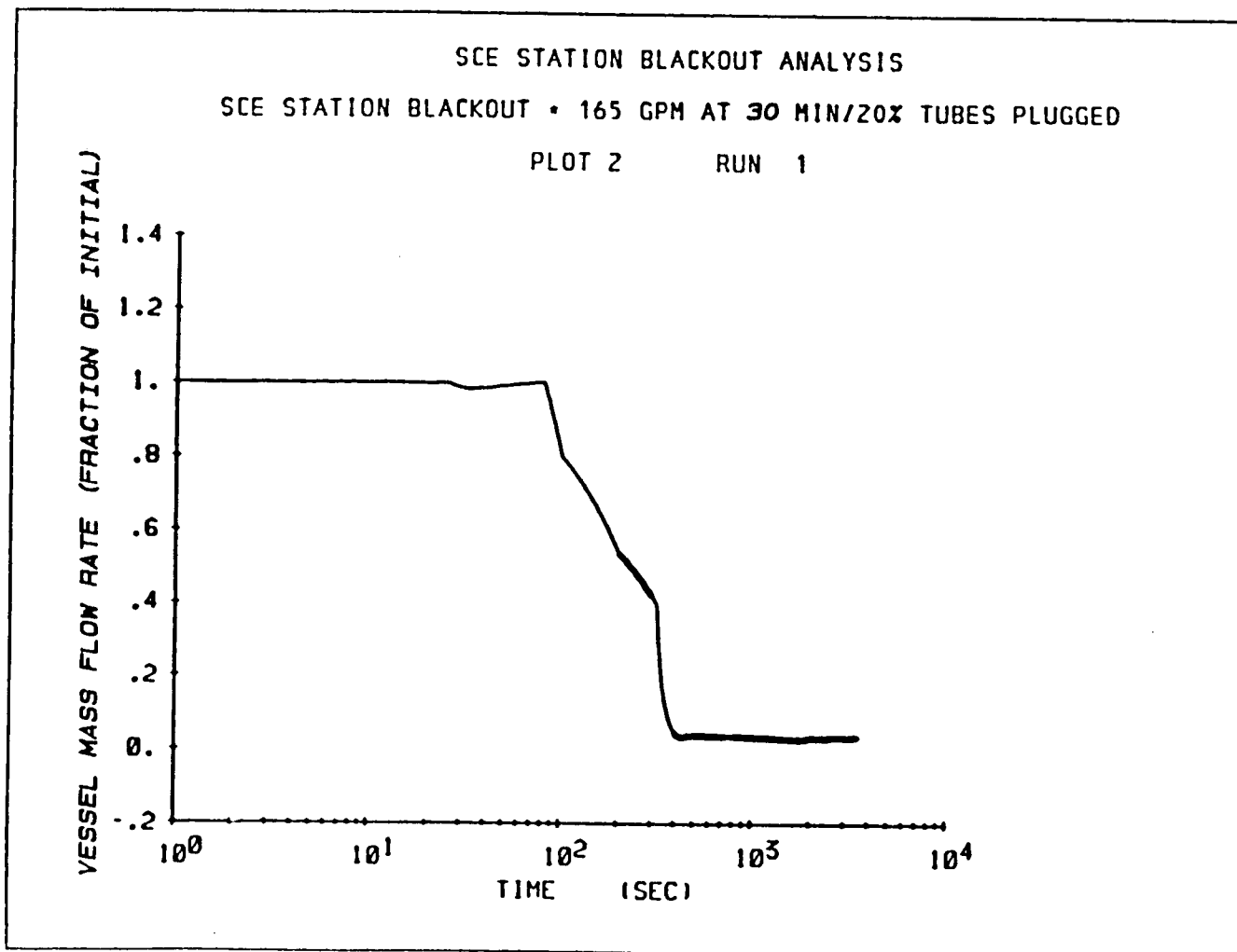


FIGURE 1-2 VESSEL MASS FLOW RATE

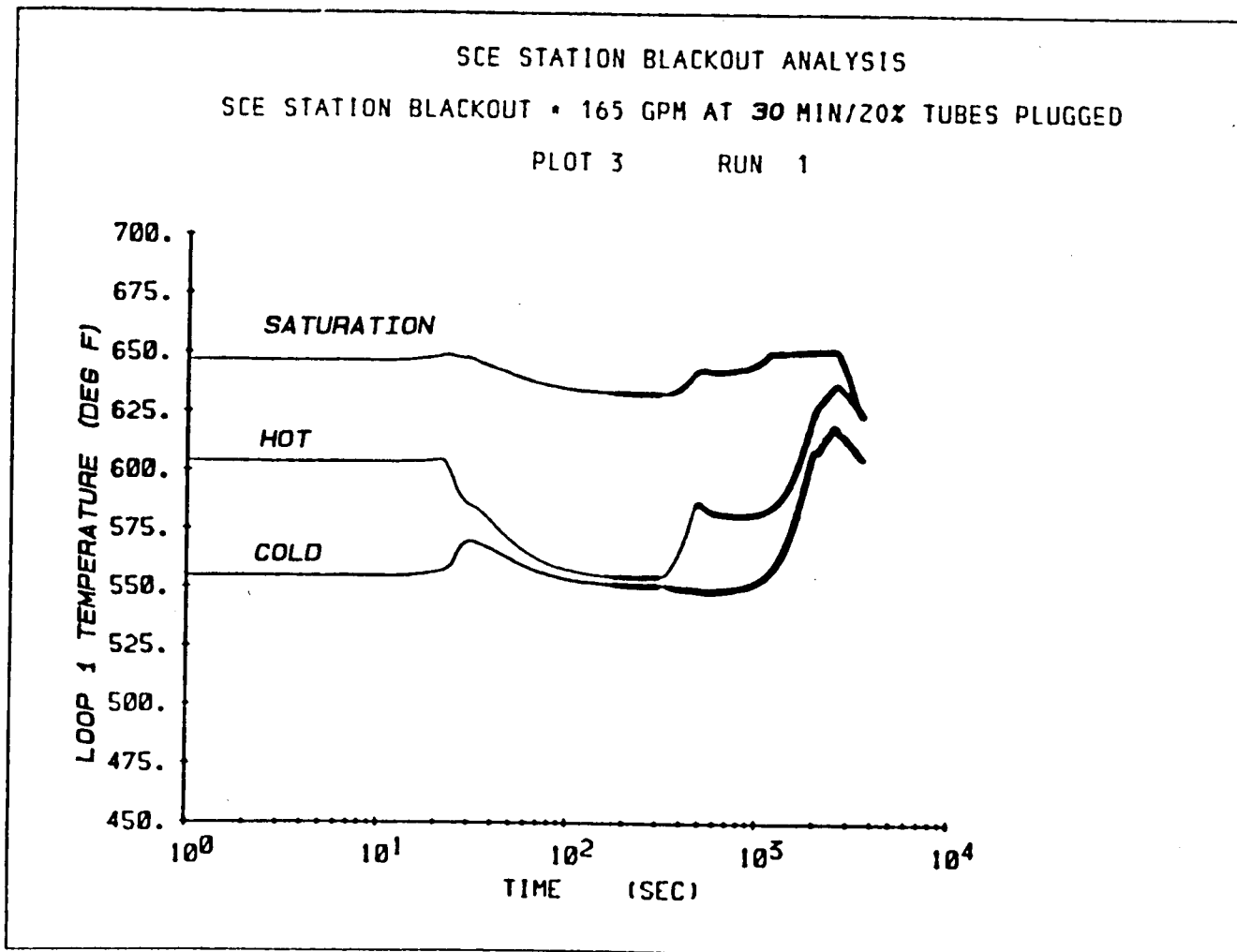


FIGURE 1-3 LOOP 1 TEMPERATURE

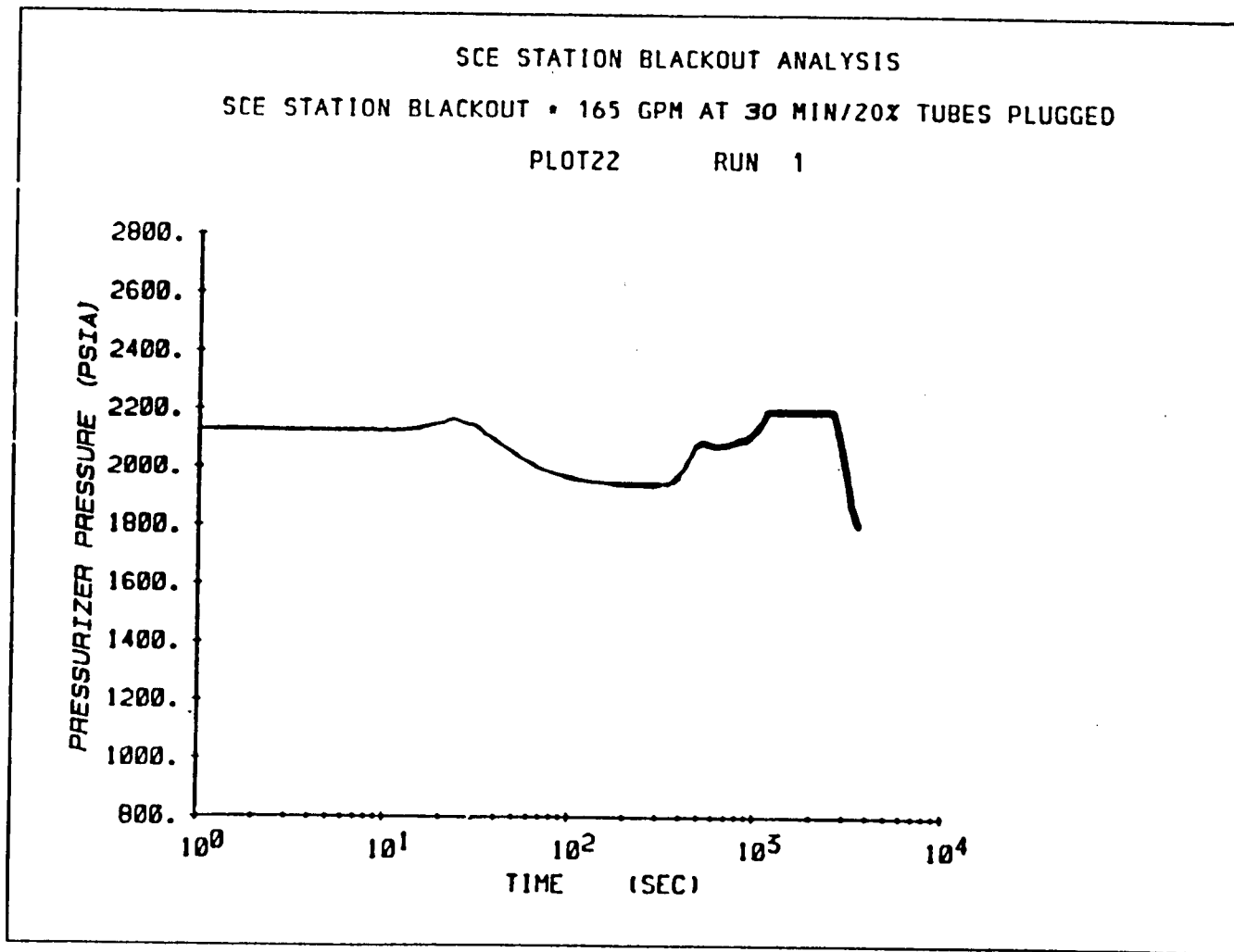


FIGURE 1-4 PRESSURIZER PRESSURE

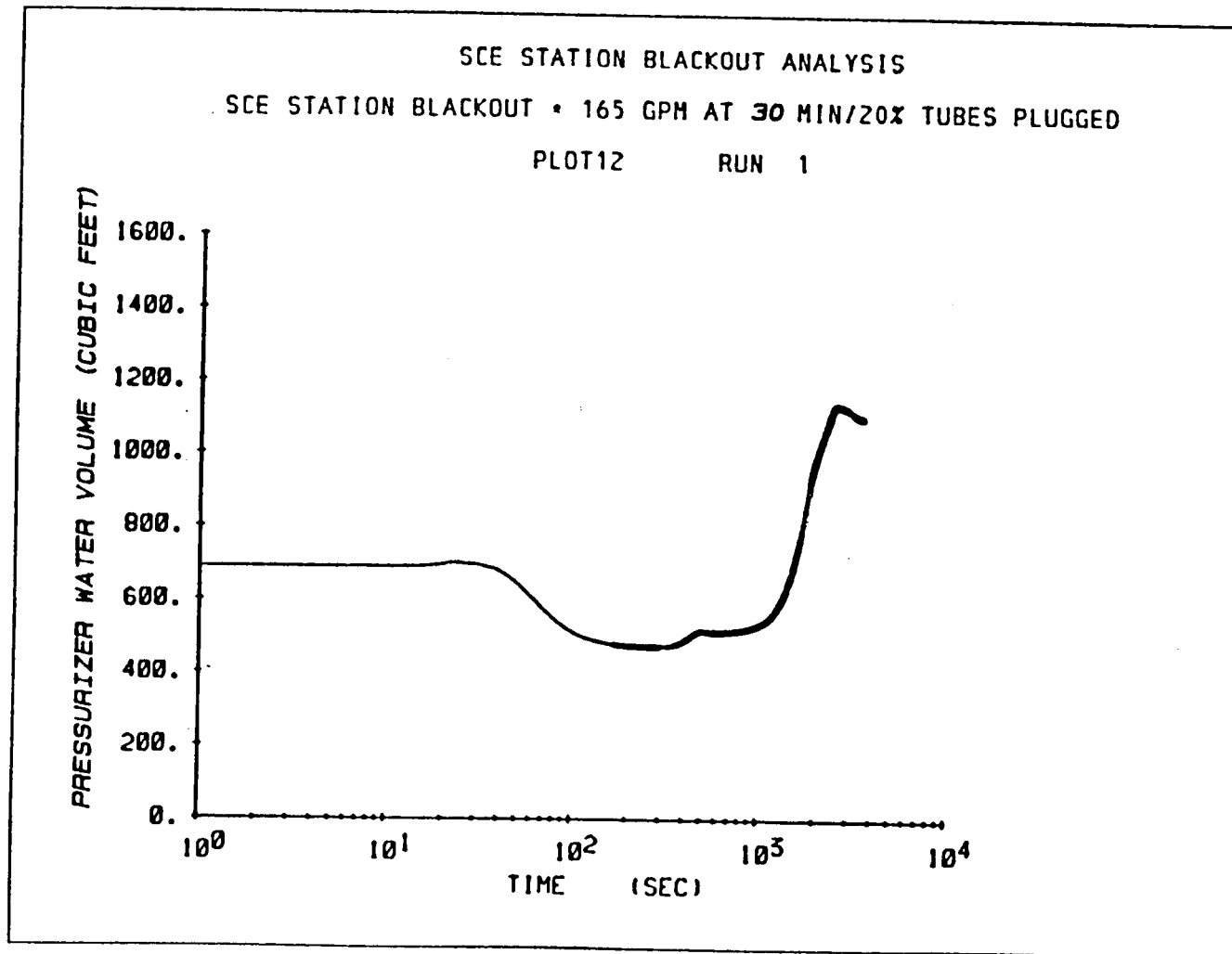


FIGURE 1-5 PRESSURIZER WATER VOLUME



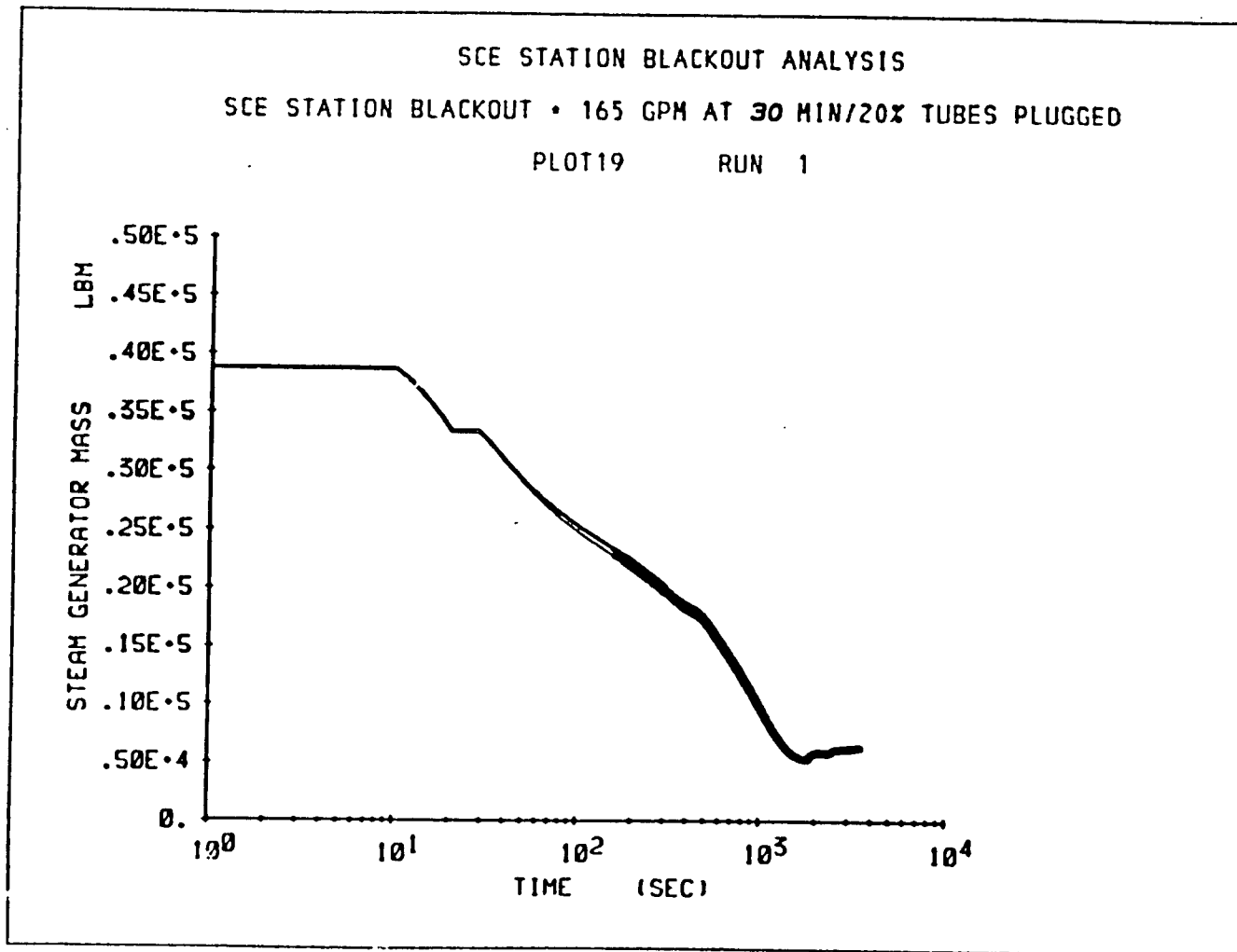


FIGURE 1-7 STEAM GENERATOR MASS

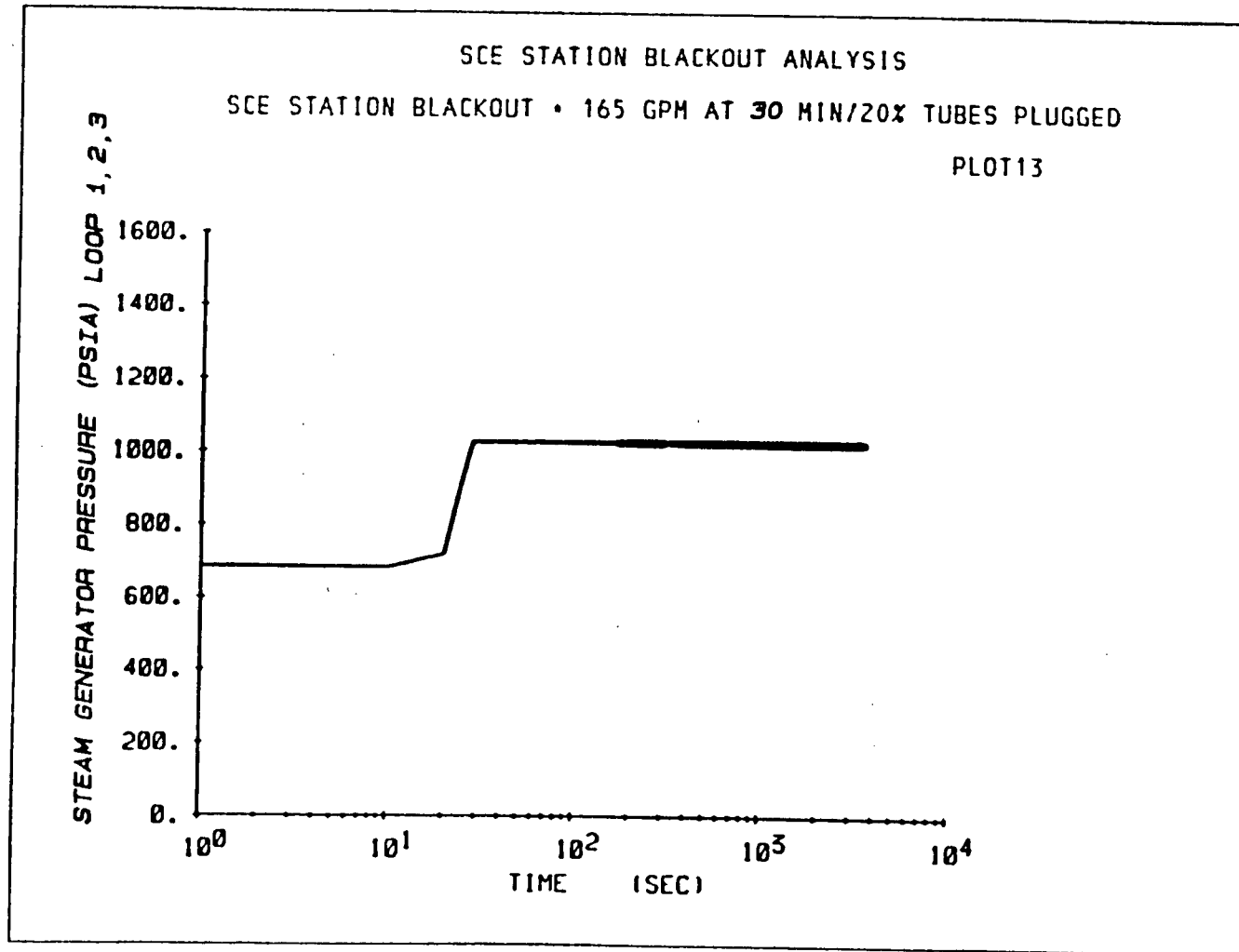


FIGURE 1-6 STEAM GENERATOR PRESSURE

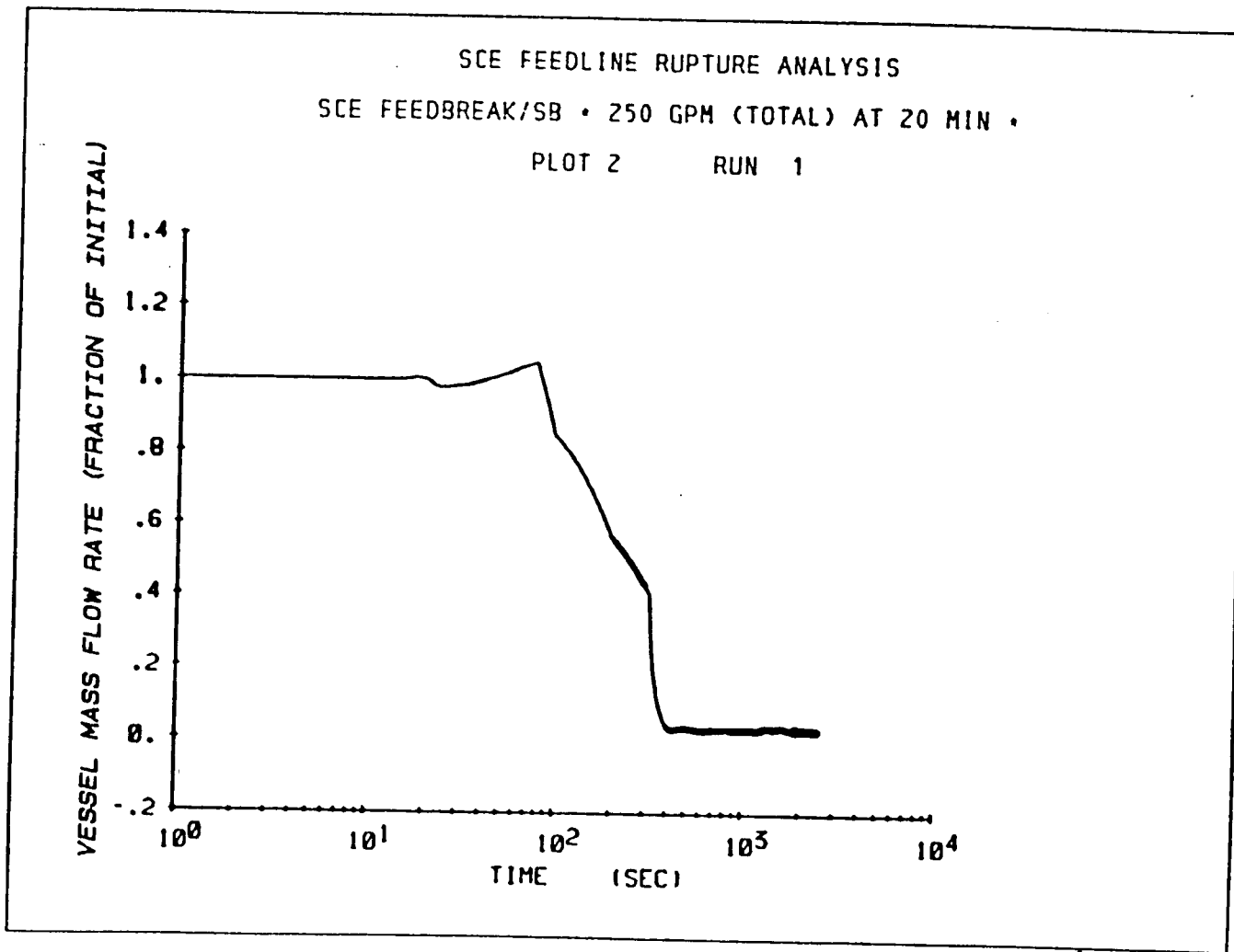


FIGURE 2-2 VESSEL MASS FLOW RATE

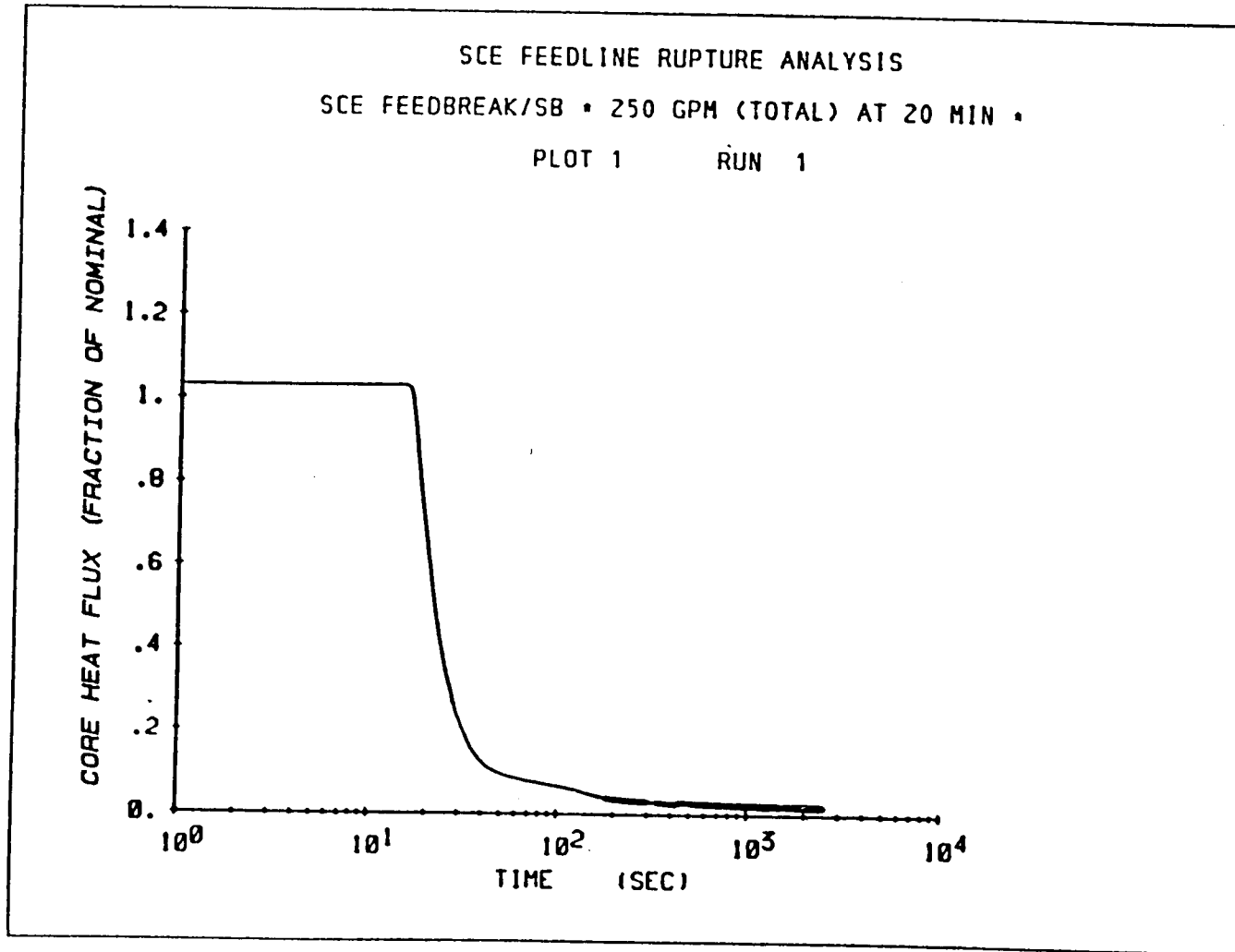


FIGURE 2-1 CORE HEAT FLUX

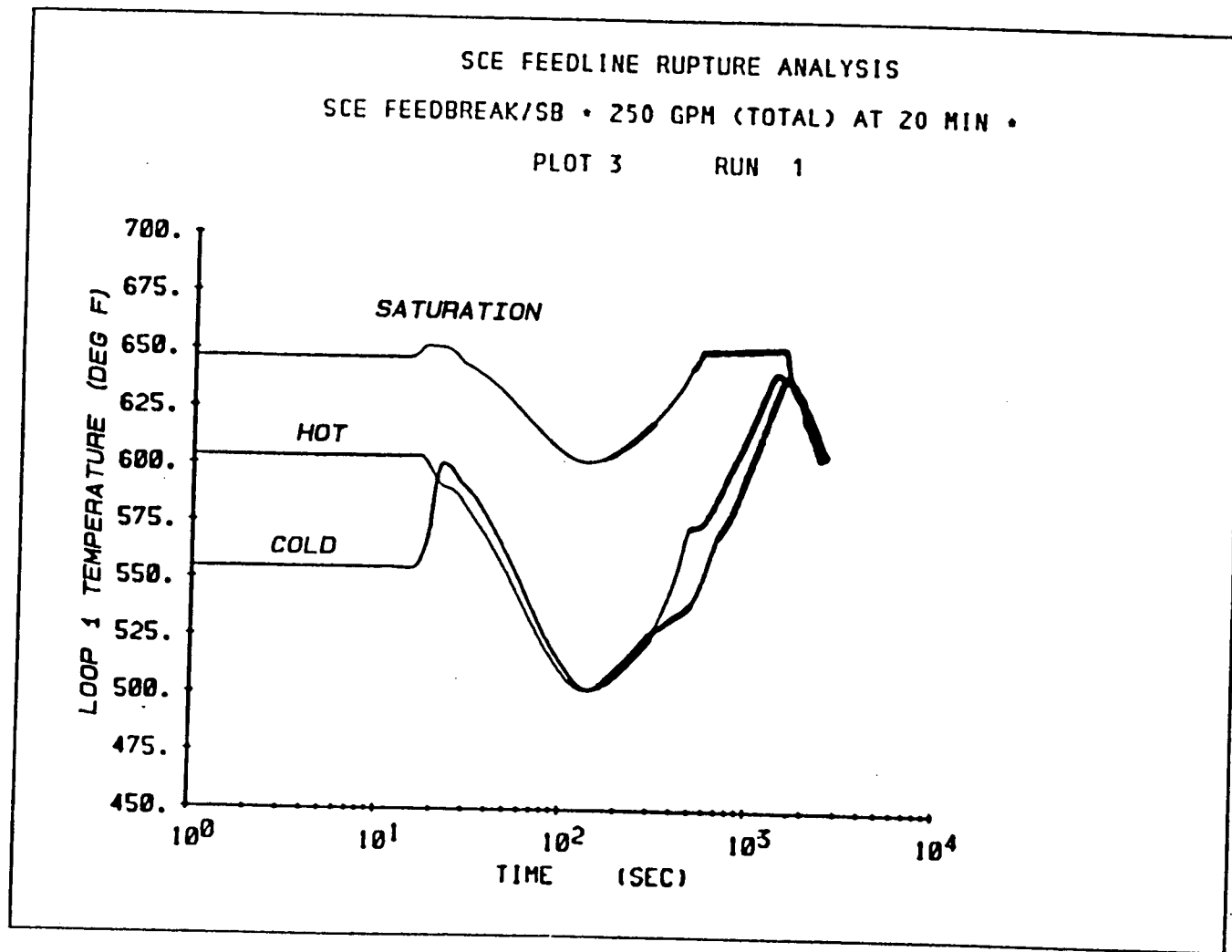


FIGURE 2-3 LOOP 1 TEMPERATURE

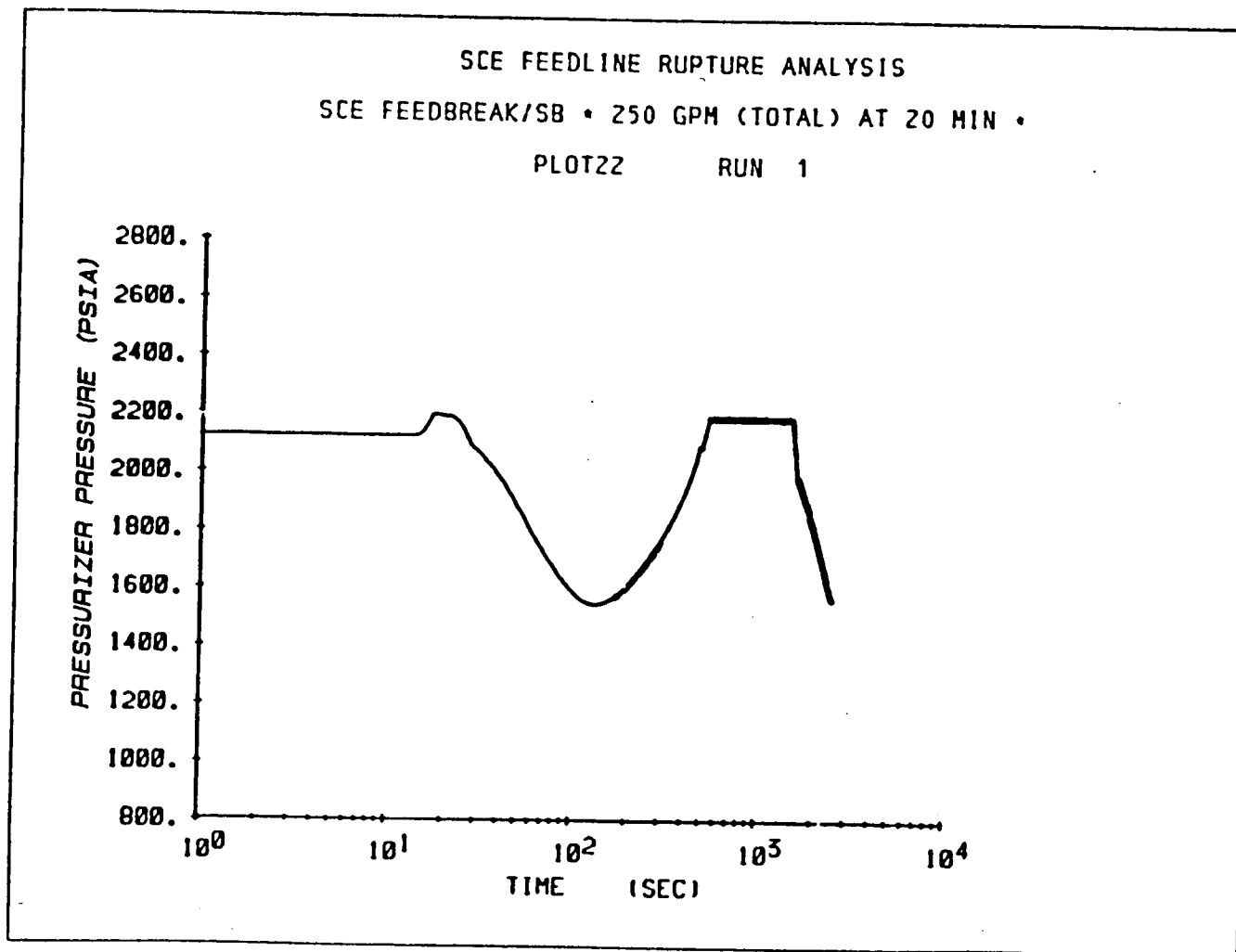


FIGURE 2-4 PRESSURIZER PRESSURE

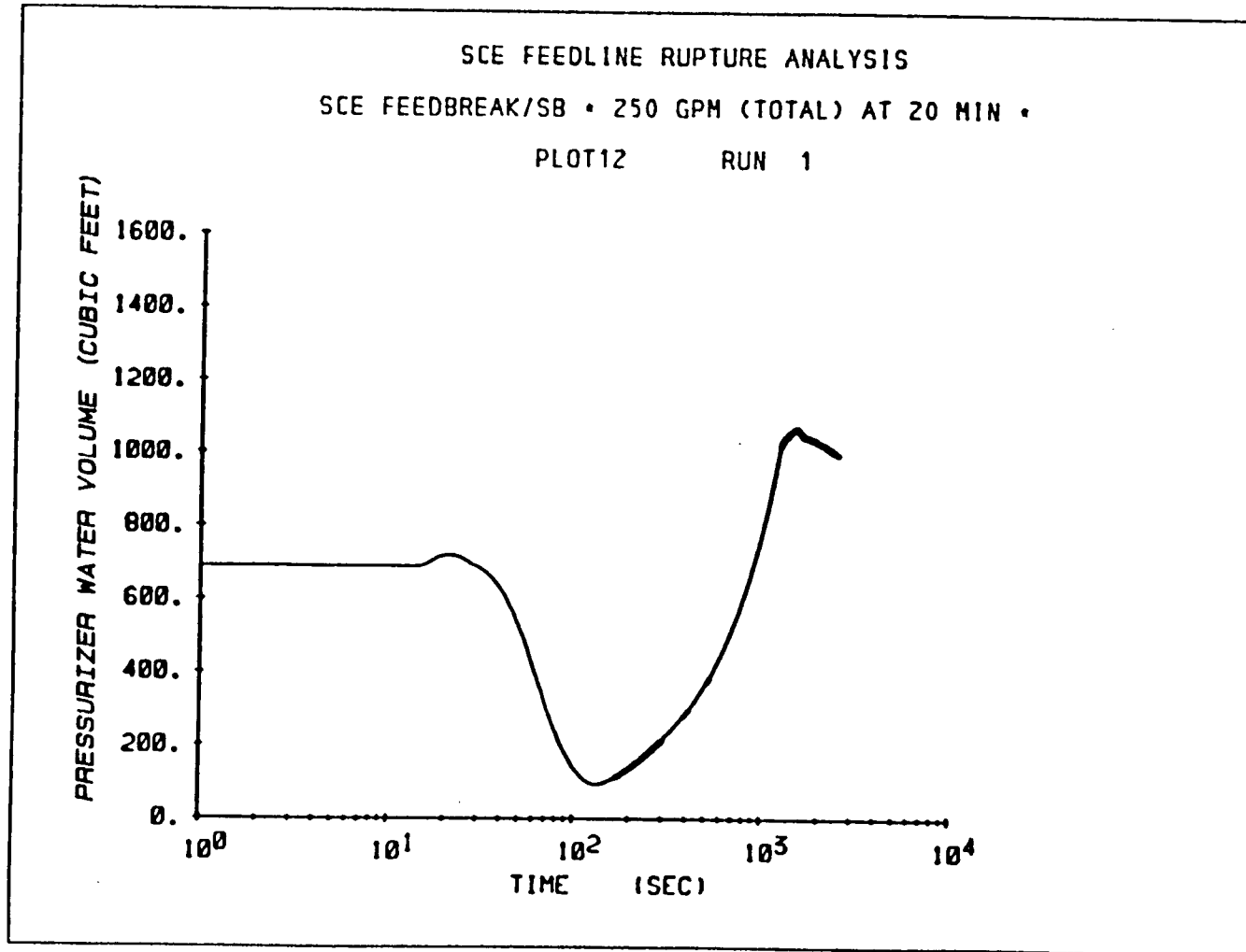


FIGURE 2-5 PRESSURIZER WATER VOLUME

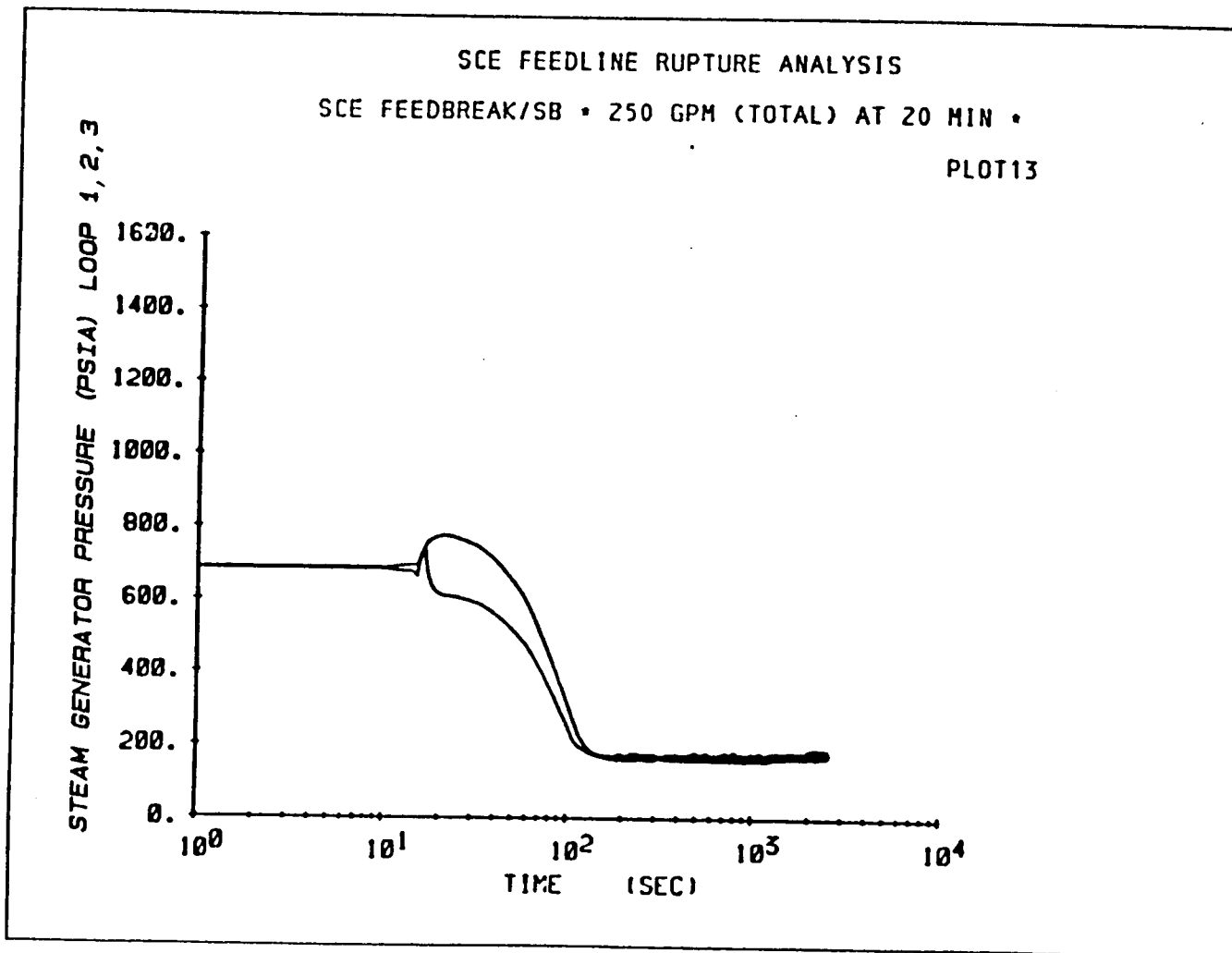


FIGURE 2-6 STEAM GENERATOR PRESSURE



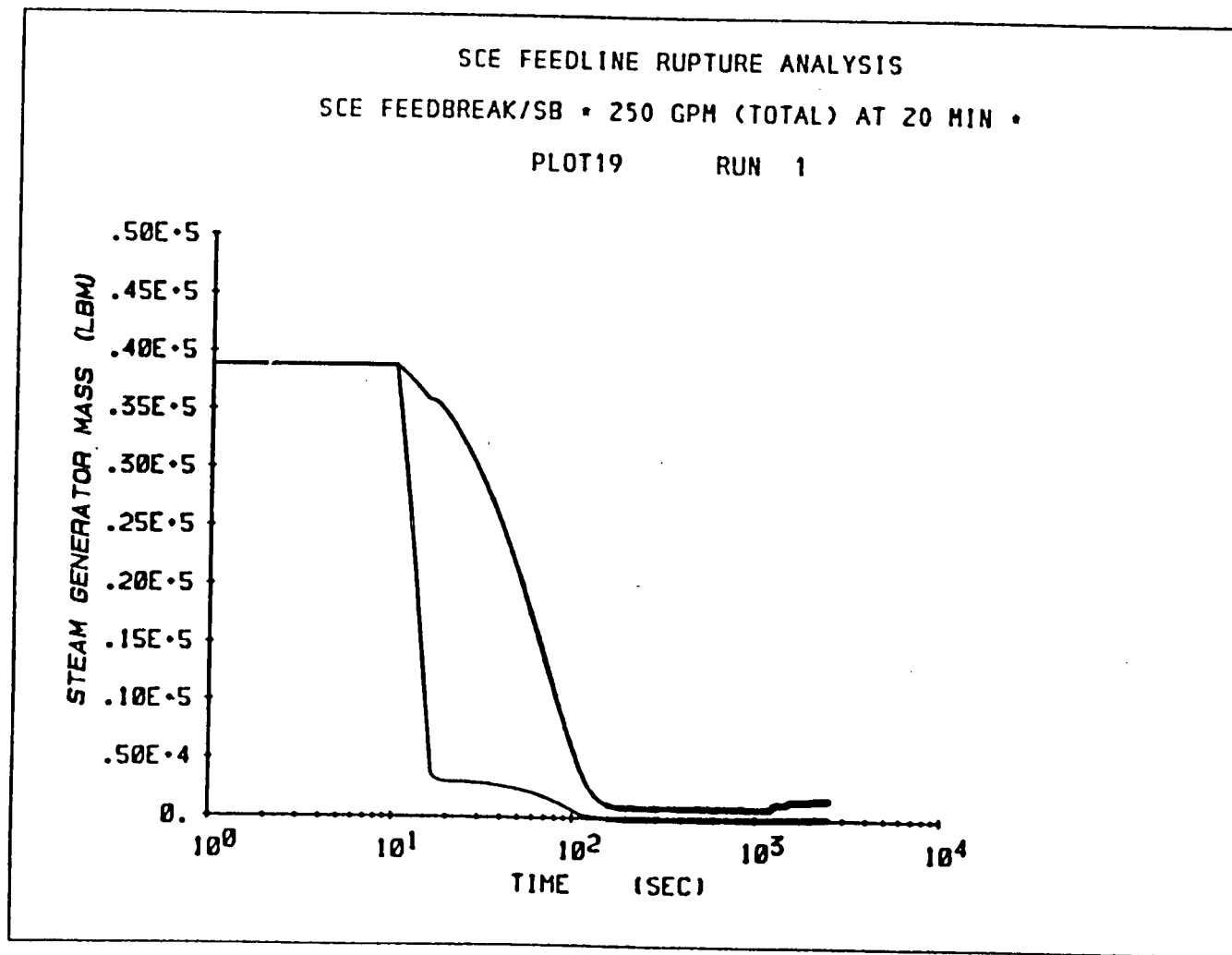


FIGURE 2-7 STEAM GENERATOR MASS

QUESTION NO. 10

Document the basis for your conclusions stated in the March 5, 1986 meeting regarding the possible effects on the November 21, 1985 event if the diesel generators had been designed to automatically load upon loss of offsite power.

RESPONSE

The conclusion stated by SCE in the March 5, 1986 meeting was that the effect which would have resulted had the diesel generators automatically loaded upon loss of offsite power would not have differed from the actual event. The basis for this conclusion is the fact that the steam generator feedwater lines voided in approximately one minute subsequent to the rupture in the east condensate train. Thus, automatic loading of the diesel generators would not have prevented the voiding but would merely have reduced the length of time feedwater and AC power was lost. The consequences would have remained unchanged.

The time required to void the steam generator feedwater lines was determined by calculation. A total leakage area of 3 square inches is estimated based upon leakage from tubes in the first point feedwater heater and the evaporator condenser.

The damage to the evaporator condenser was discussed in our Investigation Report submitted by letter dated April 8, 1986. However, the report itself incorrectly states that helium leak checks were performed on all the other heaters and that no leakage/damage which was found could be attributed to the event (page 6-136). In fact, a helium leak check performed on the first point feedwater heater indicated the presence of a large tube leak.

Based upon the estimated leakage area and the steam generator pressure, a critical flow was developed from which a blowdown rate was calculated. It was thus determined that the feedwater lines voided in a time period on the order of one minute.

QUESTION NO. 11

Document the operator actions needed to:

- a. Transfer loads from the onsite power sources (diesels) back to an offsite power source when offsite power is recovered, and
- b. load the diesel generators to provide motive power to the electric-driven auxiliary feedwater pump in case of loss-of-offsite power.

RESPONSE

Design changes made as part of the corrective action from the SCE analysis result in differences between those operator actions which would have been required during the event and those actions which would be required after return to service. The following information addresses both cases.

The San Onofre Unit 1 diesel generators (DG) have two alternative modes of operation: isochronous and droop. In picking up a dead bus (either manually or automatically), isochronous control is required for speed regulation. In paralleling the DG with the offsite power system, droop is required in order to have load control. After design changes are made during this outage, the diesel will automatically transfer to the droop mode when ever it is paralleled to the offsite power system through either the A, B or C transformer. The existing design (and the operating procedures) does not provide for changing from isochronous to droop control when the DG is loaded.

With the present design, the loads from the onsite power sources cannot be transferred back to an offsite power source by paralleling buses. Restoration of offsite power by drop (deenergization) and pickup is described as follows:

- Verify offsite power is available
- Verify plant conditions permit momentary deenergization of the effected 4 kV bus
- If reconnecting to "C" transformer, ensure reactor bypass breaker closed
- Open DG output breaker
- Synchronize and close offsite power source 4 kV breaker
- Verify 4 kV bus is energized
- Complete shutdown of diesel generator
- Repeat sequence for a second train if required

After completion of the design changes, the loads from the onsite power sources will be transferred back to the offsite power system by paralleling. No interruption in the operation of in-plant equipment will occur. The operator actions required will be similar to the following:

Verify offsite power is available  
 Synchronize the diesel to the offsite power system using the bus main or tie breaker  
 Verify offsite power connected  
 Open DG output breaker  
 Close reactor bypass breaker (if open)  
 Complete shut down of diesel generator  
 Repeat sequence for second train if required

With respect to operator action required to power the motor-driven AFW pump from the DG's upon loss of offsite power, reference is made to Emergency Operating Instruction (EOI) SO1-1.0-60, "Loss of All AC Power." Step 1 of the EOI directs the operators to verify offsite power available (i.e., in the switchyard). If offsite power is unavailable, the operator is directed to align the DG to the 4 kV system using the following steps:

<u>Present</u>	<u>After DCP</u>
Verify DG is running	Verify DG is running
Ensure 4 kV bus source breakers are open	Ensure 4 kV bus is isolated (tie and main breaker is open)
Open 4 kV bus tie breakers	Reset LOP
Open C transformer reactor bypass breakers	Close DG output breaker
Reset LOP at the sequencer panel	Verify 4 kV bus energized
Close DG output breaker	
Verify 4 V bus is energized	

Upon re-energizing the 4 kV bus, the motor-driven AFW pump would automatically start if a low steam generator level signal is present.

Subsection 8.1.3, Hardware Changes, of SCE's April 8, 1986 report provides a summary of hardware changes which will be completed prior to return to service. Item 12 of this list states:

"The diesel governor control will be modified so that it switches automatically from the isochronous mode to the droop mode whenever the associated bus is paralleled with the offsite power system through the A, B or C auxiliary transformers. (The speed control will automatically switch back to isochronous whenever the parallel with the offsite power system is broken). This eliminates the need to deenergize the bus in order to transfer it from the diesel to an offsite source."

The motor-driven AFW logic will remain unchanged, starting automatically in the presence of a low steam generator level signal.

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ENCLOSURE 2

RESPONSES TO APRIL 21, 1986 LETTER

QUESTION NO. 1

What are the new locations of the 10-inch feedwater system check valves relative to the flow control valve upstream and the block valve downstream? The Isometric Drawings previously provided only show the original locations.

RESPONSE

Figures 1, 2 and 3 are IDCN's from DCP 3400.30 BM which relocate the check valves 4' - 6-3/4" downstream of the reducer of each flow control valve and 0' - 7" from the downstream block valve. The offsite test program modeled this configuration.



INTERIM INFORMATION ONLY  
 DESIGN CHANGE NOTICE  
 AREA 2 (IDCN)

IDCN NUMBER 5-4

DOCUMENT NO.	SHEET NO.	REV NO.	DCN CONV		QUALITY CLASS
			DATE	DOC REV SUB NO.	
334539	-	2			SK

SUPPLEMENTAL PAGE

**AFTER**

JOB NO. 15691-791 PAGE 4 OF 8 PAGE

DATE: 3/29/86 BY: F. GOPAK

DESCRIPTION OF CHANGE

MODIFY FEEDWATER PIPING  
 DOWNSTREAM OF FLOW CONTROL  
 VALVE. ASSIGN SECTION   
 WELD IDENTIFIERS

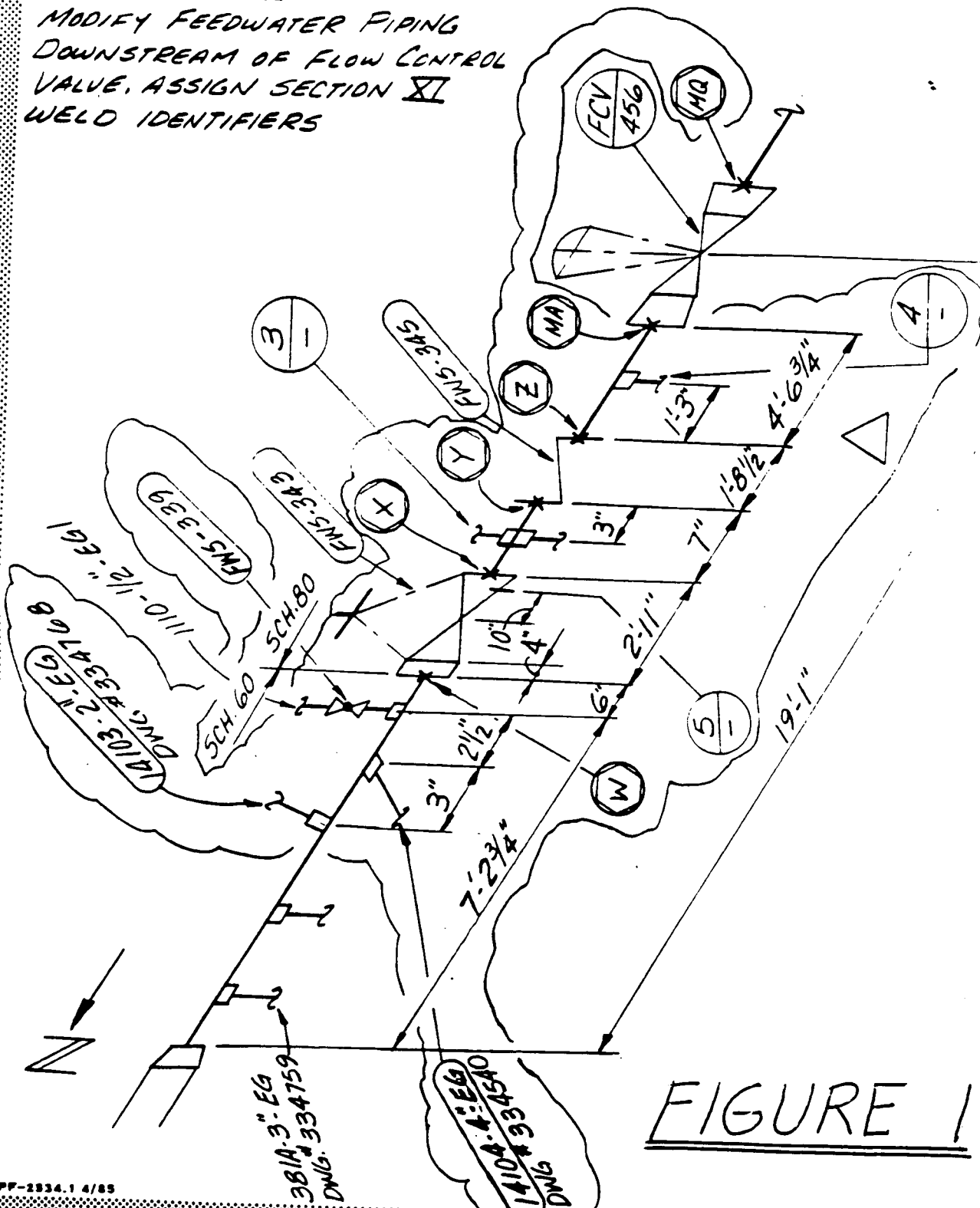


FIGURE 1

INFORMATION ONLY

INFORMATION ONLY

DCP 3400.308M REV A SHEET 4 OF 8

PF-2834.1 4/85

96

PF-5396 (10079) 4/84



INFORMATION ONLY  
 DESIGN CHANGE NOTICE  
 (IDCN)

IDCN NUMBER 5-4

DOCUMENT NO.	SHEET NO.	REV NO.	DCN CONV.		QUALITY CLASS
			DATE		
			DOC REV	SUB NO	
334538	-	3			SREAN

SUPPLEMENTAL PAGE

AREA 2

JOB NO. 15691-791 PAGE 4 OF 7 PAGE

DATE: 3/27/86 BY: E. HOLGUIN

DESCRIPTION OF CHANGE

MODIFY FEEDWATER PIPING DOWNSTREAM OF FLOW CONTROL VALVE. ASSIGN SECT. II IDENTIFIERS.

AFTER



DCP 3400.308M REV A SHEET 1 OF 1

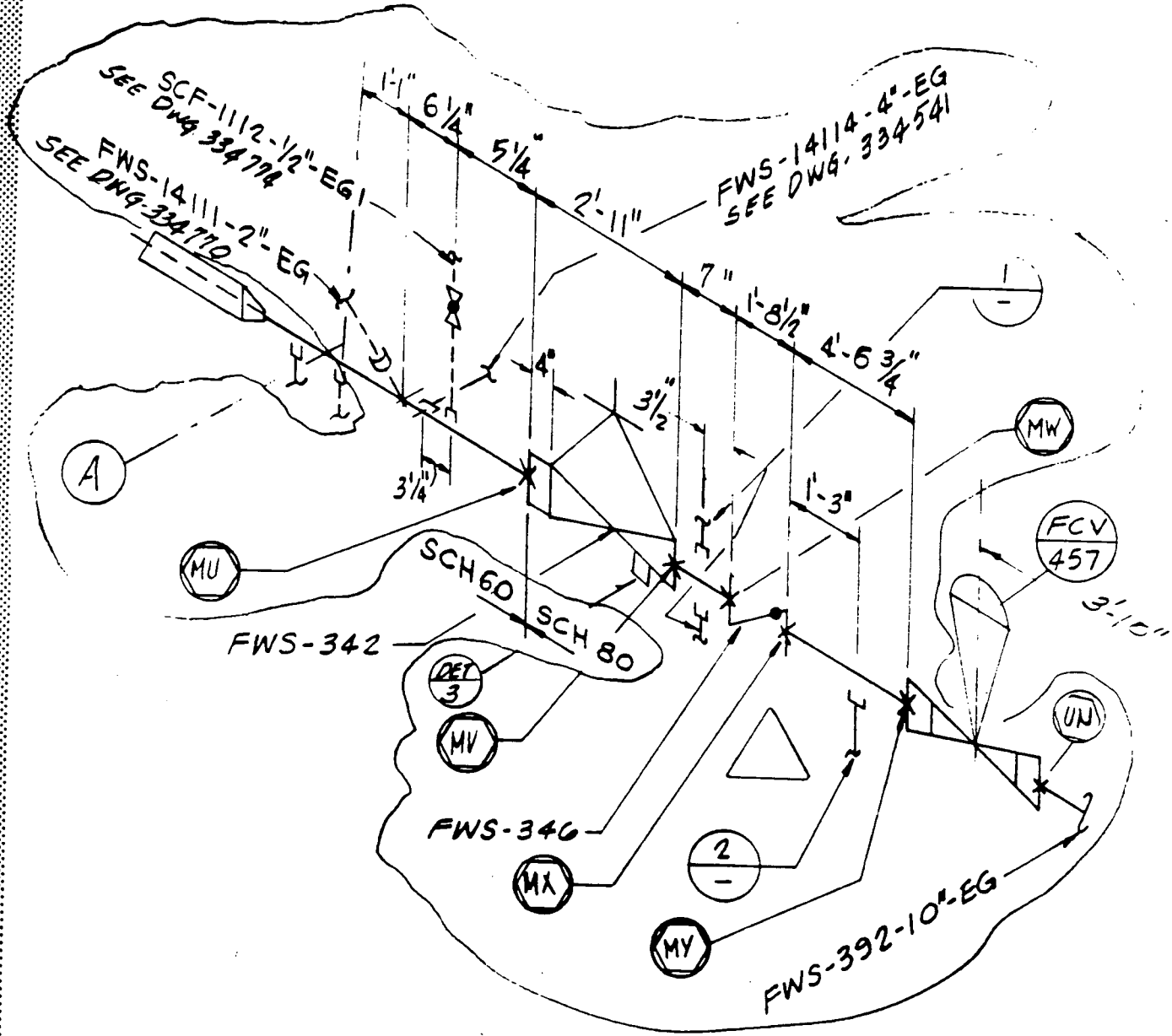


FIGURE 2

PF-2834.1 4/85

INFORMATION ONLY





QUESTION NO. 2

With regard to your current IST program, it appears that at least some of the five check valves which failed can be (and have been) tested while the plant is hot. However, relief from the Code has been requested for these valves to only test during cold shutdown. What is the basis for the reduced periodicity of testing these valves in light of the code requirements and the recent failures?

RESPONSE

The five check valves mentioned above are presently tested (closed direction) in Mode 3 to provide the necessary differential pressure to assure closure. Relief from the ASME Code testing frequency was requested because the valves cannot be tested quarterly in Mode 1. The term "cold shutdown" as it is used in the IST program actually means Modes 3-5 since not all "cold shutdown" valves can actually be tested in Mode 5. It is our intended practice to initiate "cold shutdown" testing within 48 hours of entry into Mode 3 for valves required to be tested in Mode 3, within 48 hours of entry into Mode 4 for valves required to be tested in Mode 4, and within 48 hours of entry into Mode 5 for values required to be tested in Mode 5. All initiated testing would continue until complete, i.e., all valves tested within the last 92 days, or the unit is ready to return to Mode 1. The IST procedures will be revised to more clearly identify this intent. Typically, valves are tested based on previous test date, that is, the most recently tested valve is tested last and the valve with the longest interval since its previous test is tested first. The previously submitted ASME Code relief request will be clarified to more clearly identify the intended testing conditions as specified above.

QUESTION NO. 3

What enhanced testing is planned for each of the new Atwood-Morrill check valves, including any quantitative leak rate criteria, procedures, and how new testing taps will be utilized?

RESPONSE

Demonstration testing has been and will be performed on the Atwood-Morrill check valves by Drs. Paul Tullis and William Rahmeyer (Utah State University Foundation). The first phase of testing was completed during the week of March 31, 1986 and included flow stability tests. The second phase of testing will be performed later this year and will involve accelerated wear tests. It is expected that the testing will be completed in August, 1986, with the final report completed approximately 45 days following test completion.

Quantitative leak rate criteria have been developed and are included in the guidelines (Attached). The guidelines also describe how the new test taps will be utilized. Station personnel are presently using the test guidelines to develop comprehensive procedures for testing the valves.

# ATTACHMENT 1

Enclosure  
Page 1 of 10  
March 11, 1986  
Log BPC/SCE-86-3924

## TEST PROCEDURE GUIDELINE FOR CHECK VALVES LEAKAGE RATE TEST

### I. Functional Test for Check Valves FWS-006, FWS-007 and FWS-012 Inside the Containment:

A. Objective: To verify that the check valve back leakage rates are within the allowable limits. Correct deficiencies if required.

#### B. References:

1. P&ID 5178225, Revision 4, Main Steam System
2. P&ID 5178206, Revision 3, Feedwater System

#### C. Prerequisites:

1. Completion of check valve installation.
2. Verify calibration of pressure gauges.
3. Test to be done during Mode V or VI.
4. Isolation valves (FWS-343, FWS-377, FWS-339, AFW-325, FWS-342, FWS-376, FWS-352, AFW-326, FWS-396, FWS-415, FWS-382 and AFW-328) upstream of the check valves are closed.
5. Establish that the feedwater level of the steam generator at the feed ring elevation  $\pm 2^{+0}$ .

6. Nitrogen system blanket is established per procedure.

D. Acceptance criteria: Check valves back leakage rate is within 0.48 gallons per minute at 150 psig. This test procedure was written for testing at 150 psig. Alternate test pressures can be used. The acceptance criteria for using the alternate shall follow the equation.

Allowable leak rate at pres. P,  $Q = 0.48 \sqrt{\frac{P}{150}}$  (gpm), see Fig. 2.

The allowable fluctuation in the test pressure is  $\pm 5$  psi or  $\pm 10\%$  whichever is greater. If test pressures less than 150 psig are used, functional testing of the feedwater main and bypass valves must be done at a test pressure of 150 psig (Test II).

#### E. Method

1. Test the check valve one at a time only. Close isolation valves upstream of the check valve.
2. Connect measuring hose at the designated drain connection (see Table 1) upstream of the check valve. Make sure that the highest point of the connected measuring hose has a minimum loop as it is shown in Fig. 1.

3. Open drain valve (FWS-337, FWS-338, FWS-340, FWS-426 and FWS-424) to depressurize the isolated line upstream of the check valve to atmospheric conditions. To confirm that the upstream isolation valves do not leak, monitor and maintain atmospheric reading on the gauges on the main feedwater and auxiliary feedwater pumps.
  4. Using nitrogen, pressurize the steam generator downstream of the check valve (if pressure is not already established). Monitor and maintain steam generator pressure at 150 psig minimum to 165 psig.
  5. At steady state, and using a container of known volume, measure and record the check valve back leakage rate by measuring the time required to accumulate one gallon. Take two measurement test readings for comparison.
  6. After measuring the check valve back leakage rate, close the nitrogen pressurizing line (if not required for other than testing).
  7. Making sure the system is vented, close the drain valves and disconnect the measuring hose.
  8. Open back all the isolation valves that were closed during the test.
- F. Alternate method for functional test of FWS-006, FWS-007 and FWS-012:

Performance of this test is subject to the availability of the auxiliary feedwater pumps as a pressurization source.

1. With a nitrogen blanket established, initiate auxiliary feedwater flow to pressurize the steam generator. When a test pressure has been established, perform the back leak rate test in accordance with E1 through E5 above. As the pressure will decay during the test, the following requirements apply to the test pressure:
  - a. The decay in steam generator pressure shall be no more than 10% of the final pressure.
  - b. For the purpose of determining the allowable leak rate, the final measured steam generator pressure shall be used.

NOTE: The allowable leakage rate shall be determined using the minimum pressure value obtained during the test.

II. Functional Test for Check Valves FWS-345, FWS-346, FWS-398, FWS-379, FWS-378, FWS-419 in the feedwater system.

A. Objective: To verify that the feedwater system check valves back leakage rates are within the allowable limit. Correct deficiencies if required.

B. Reference:

1. P&ID 5178206, Revision 4, Feedwater System.

C. Prerequisites:

1. Completion of check valve installation.
2. Verify calibration of pressure gauges.
3. Isolation valves (FWS-343, MOV-21, FWS-377, FWS-381, FWS-342, MOV-20, FWS-376, FWS-372, FWS-396, MOV-22, FWS-415 and FWS-419) upstream and downstream of the check valves are closed.
4. Test to be done in Mode V or VI.

D. Acceptance criteria: This criteria applies to the combined check valves back leakage rates of the following paired check valves: FWS-345 and FWS-379; FWS-346 and FWS-378 and FWS-398 and FWS-417 leakage shall be less than is 0.48 gallons per minute. This procedure is written using test pressures of 150 psig. Other test pressures can be used. The allowable leak rate at other test pressures shall follow the equation

Allowable leak rate at pres. P, Q =  $0.48 \sqrt{\frac{P}{150}}$  (gpm), see Fig. 2.

If the test pressure used on the downstream check valves (Test I) is less than 150psig, this test shall be performed at 150 psig minimum.

The allowance fluctuation in the test pressure is  $\pm 5$  psi or  $\pm 10\%$  whichever is greater.

E. Method:

1. Test the check valves one at a time only. Close isolation valves upstream and downstream of the check valve.
2. Connect measuring hose at the designated drain or vent connections (see Table 1). Make sure that the highest point of the connected measuring hose has a minimum loop as it is shown in Fig. 1.
3. Open the drain or vent valve where the measuring hose is connected to depressurize the line to atmospheric conditions. To confirm the upstream isolation valves do not leak, monitor and maintain atmospheric reading on the gauges on the main feedwater pumps.

4. Connect the high pressure water supply to the drain or vent connection designated downstream of the check valve (see Table 1). The water supply must meet the requirement of the chemistry flush specification for the feedwater system. Open the drain or vent valve and high pressure water supply valve and pressurize the line. Using the pressure gauge provided in the water supply hose, maintain and monitor the pressure downstream of the check valve at 150 psig minimum to 165 psig.
5. At steady state, and using a container of known volume, measure and record the check valve back leakage rate by measuring the time required to accumulate one gallon. Take two measurement test readings for comparison.
6. After measuring the check valve back leakage rate, close the drain or vent valve where the measuring hose is connected and disconnect the hose.
7. Making sure the system water is vented, close the high pressure water supply valve and close the drain or vent line valve and disconnect the high pressure water supply.
8. Open back all the isolation valves upstream and downstream of the check valve that were closed during the test.

F. Alternate Procedure:

The back leakage rate test for the feedwater system check valves can also be done during Mode III subject to the availability of the auxiliary feedwater pump as a pressurization source. The following procedure would be used.

1. Test and isolate the check valves one at a time only. Close isolation valve upstream of the check valve.
2. Connect measuring hose at the designated drain or vent connections (see Table 1). Make sure that the highest point of the connected measuring hose has minimum loop as it is shown in Fig. 1.
3. Open the drain or vent valve where the measuring hose is connected to depressurize the line to atmospheric conditions. To confirm the upstream isolation valves do not leak, monitor and maintain atmospheric reading on the gauges on the feedwater pumps.
4. Install a temporary test pressure gauge and open the valve of the vent connection upstream of the check valve as indicated in Table 1.
5. Initiate the auxiliary feedwater pump flow to pressurize the line downstream of the check valve to within  $\pm 10\%$  of the normal operating pressure. Maintain and monitor the pressure at the test pressure gauge installed at the vent connection.

6. At steady state, and using a container of known volume, measure and record the check valve back leakage rate by measuring the time required to accumulate one gallon. Take two measurement test readings for comparison.
7. After measuring the check valve back leakage rate, close the drain or vent valve where the measuring hose is connected and disconnect the hose.
8. Close the vent connection valve where the test pressure gauge is installed and remove the gauge.
9. Open back all the isolation valves upstream of the check valve that was closed during the test.



### III. Functional Test for Check Valves FWS-438 and FWS-439 in the feedwater system.

- A. Objective: To verify that the feedwater system check valves are still intact and functional.

Correct deficiencies if required. These valves have been provided with a 9/32" orifice hole drilled in the check valve disc. Standard leak rate tests cannot be performed. This testing will determine the functionality of the check valve.

B. Reference:

1. P&ID 5178205, Revision 2, Feedwater System.

C. Prerequisites:

1. Completion of check valve installation.
2. Verify calibration of pressure gauges.
3. Isolation valves (FWS-441, FWS-469, CV-875B, HV-854B, FWS-556, FWS-440, FWS-472 and HV-854A) upstream and downstream of the check valves are closed.
4. Test to be done during Mode V or VI.

- D. Acceptance criteria: When the downstream piping is pressurized to 150 psig the upstream leakage rate is less than 20 gpm. Other test pressures can be used. The allowable leakage rate at an alternate pressure P would follow the equation

$$Q = 20 \sqrt{\frac{P}{150}} \quad (\text{GPM})$$

The allowable fluctuation in test pressure is  $\pm 5$ psi or  $\pm 10\%$  whichever is greater.

E. Method:

1. Test the check valve one at a time only. Close isolation valves upstream and downstream of the check valve.
2. Connect measuring hose at the designated drain or vent connections (see Table 1). Make sure that the highest point of the connected measuring hose has a minimum loop as it is shown in Fig. 1.
3. Open the drain or vent valve where the measuring hose is connected to depressurize the line to atmospheric conditions. To confirm the upstream isolation valves do not leak, monitor and maintain atmospheric reading on the gauges on the main feedwater pumps.

4. Connect the high pressure water supply to the drain or vent connection designated downstream of the check valve (see Table 1). The water supply must meet the requirement of the hemistry flush specification for feedwater system and can provide 20 gpm at 150 psig minimum pressure to 165 psig. Open the drain or vent valve and high pressure water supply valve and pressurize the line. Using the pressure gauge provided in the water supply hose, maintain and monitor the pressure downstream of the check valve at 150 psig minimum to 165 psig.
  5. At steady state and using a container of known volume, measure and record the check valve back leakage rate by measuring the time required to accumulate ten gallons. Take two measurement test readings for comparison.
  6. After testing, close the vent valve where the measuring hose is connected and disconnect the hose.
  7. Making sure the system is vented, close the high pressure water supply valve and close the vent line valve and disconnect the high pressure water supply.
  8. Open back all the isolation valves upstream and downstream of the check valves that were closed during the test.
- F. Alternate Method for Functional Test of FSW-438, FWS-439.

This method is subject to the availability of the feedwater pumps as a pressurization source during mode 5 or 6. Test only one check valve at a time feedwater system will be aligned such that, one feedwater pump will be run and the water will be recirculated to the condenser via the 3" miniflow line. The check valve on the discharge of the out-of-service feedwater pump will be tested as follows;

1. Establish feedwater flow and flow path form one feedwater pump close the upstream isolation valve on the check value: on the discharge of tag out-of-service pump.
2. With the flow path in the crosstie between the feedwater heaters open, install a temporary pressure gauge on the pressurized side of the check value.
3. Connect measuring hose at the designated drain or vent connections (see Table 1). Make sure that the highest point of the connected measuring hose has a minimum loop as it is shown in Figure 1
4. Open the drain or vent valve where the measuring hose is connected to depressurize the line to atmospheric conditions.
5. At steady state, and using a container of known volume, measure and record the check valve leakage rate by measuring the time required to accumulate 20-40 gallons.

6. After measuring the check valve back leakage rate, close the drain or vent valve where the measuring hose is connected and disconnect the hose.
7. Making sure the system is vented, terminate Feedwater miniflow.

CAUTION: Care should be taken when performing this alternate testing, as the potential exists for overpressurization of the feed water suction piping. The suggested test pressure is 150 psig.

IV. Functional Test for Check Valves AFW-321, AFW-322, AFW-324, in the Auxiliary Feedwater Systems. (Continued)

B. Reference: P&ID 5178220, Revision 5 Auxiliary Feedwater System.

C. Prerequisites:

1. Completion of check valve installation.
  2. Verify calibration of pressure gauges.
  3. Isolation valves( AFW-325, FCV-2300, AFW-326, FCV-3301, FCV-2301, AFW-338, FCV-3300,) upstream and downstream of the check valve are closed.
  4. Test to be during Mode V or VI.
- D. Acceptance criteria: Check valve back leakage rate is within 0.48 gallons per minute. This procedure is written using test pressures of 150 psig. Other test pressures can be used. The allowable leak rate at other test pressures shall follow the equation.

Allowable leak rate at pres. P, Q =  $0.48 \sqrt{\frac{P}{150}}$  (gpm), see Fig. 2.

The allowable fluctuations in test pressure is  $\pm 5$ psi or  $\pm 10\%$  whichever is greater.

E. Method:

1. Test check valve one at a time only. Close isolation valves upstream and downstream of the check valve.
2. Connect measuring hose at the designated connections upstream of the check valve (see Table 1). Make sure that the highest point of the connected measuring hose has a minimum loop as it is shown in Fig. 1 is higher than the highest point of the isolated line where it is connected (see Fig. 1).
3. Open the drain or vent valve where the measuring hose is connected to depressurize the line to atmospheric condition. To confirm the upstream isolation valves do not leak, monitor and maintain atmospheric reading on the gauges on the auxiliary feedwater pumps.
4. Connect the high pressure water supply to drain or vent connection designated downstream of the check valve (see Table 1). The water supply must meet the requirement of the chemistry flush specification for the feedwater system. Open the drain or vent valve and the high pressure water supply valve and pressurize the line. Using the pressure gauge provided in the water supply hose, maintain and monitor pressure downstream of the check valve at 150 psig to 165 psig.

5. At steady state, using a container of known volume, measure and record the check valve back leakage rate by measuring the time required to accumulate one gallon and the check valve minimum downstream pressure value. Take two measurement test readings for comparison.
6. After measuring the check valve back leakage rate, close the valve where the measuring hose is connected and disconnect the hose.
7. Making sure the system is vented, close the high pressure water supply valve and close the vent or drain valve where high pressure water supply is connected and disconnect the high pressure water supply line.
8. Open back all the isolation valves upstream and downstream of the check valve that were closed during the test.

TABLE 1

CHECK VALVE	HIGH PRESSURE SUPPLY CONN.	MEASURING CONNECTION	ISOLATION VALVES
FWS-006		FWS-338	FWS-376, AFW-326, FWS-352 and FWS-342
FWS-007		FWS-337	FWS-339, FWS-377, FWS-343 and AFW-325
FWS-012		FWS-424	FWS-382, FWS-396, FWS-415 and AFW-328
FWS-417	FWS-432	FWS-423	FWS-415 and FWS-419
FWS-398	FWS-368	FWS-365	FWS-396 and MOV-22
FWS-378	FWS-428	FWS-422	FWS-376 and FWS-372
FWS-346	FWS-446	FWS-366	FWS-342 and MOV-20
FWS-379	FWS-423	FWS-421	FWS-377 and FWS-381
FWS-345	FWS-425	FWS-367	FWS-343 and MOV-21
FWS-439	FWS-445	FWS-565	HV-854B, HV-852B, CV-875B and FWS-473
FWS-438	FWS-540	FWS-510	FWS-440, FWS-556, FWS-472 and HV-854A
AFW-321	DRAIN	VENT	AFW-325 and FCV-2300
AFW-322	DRAIN	VENT	AFW-326, FCV-3301 and FCV-2301

(2002k)

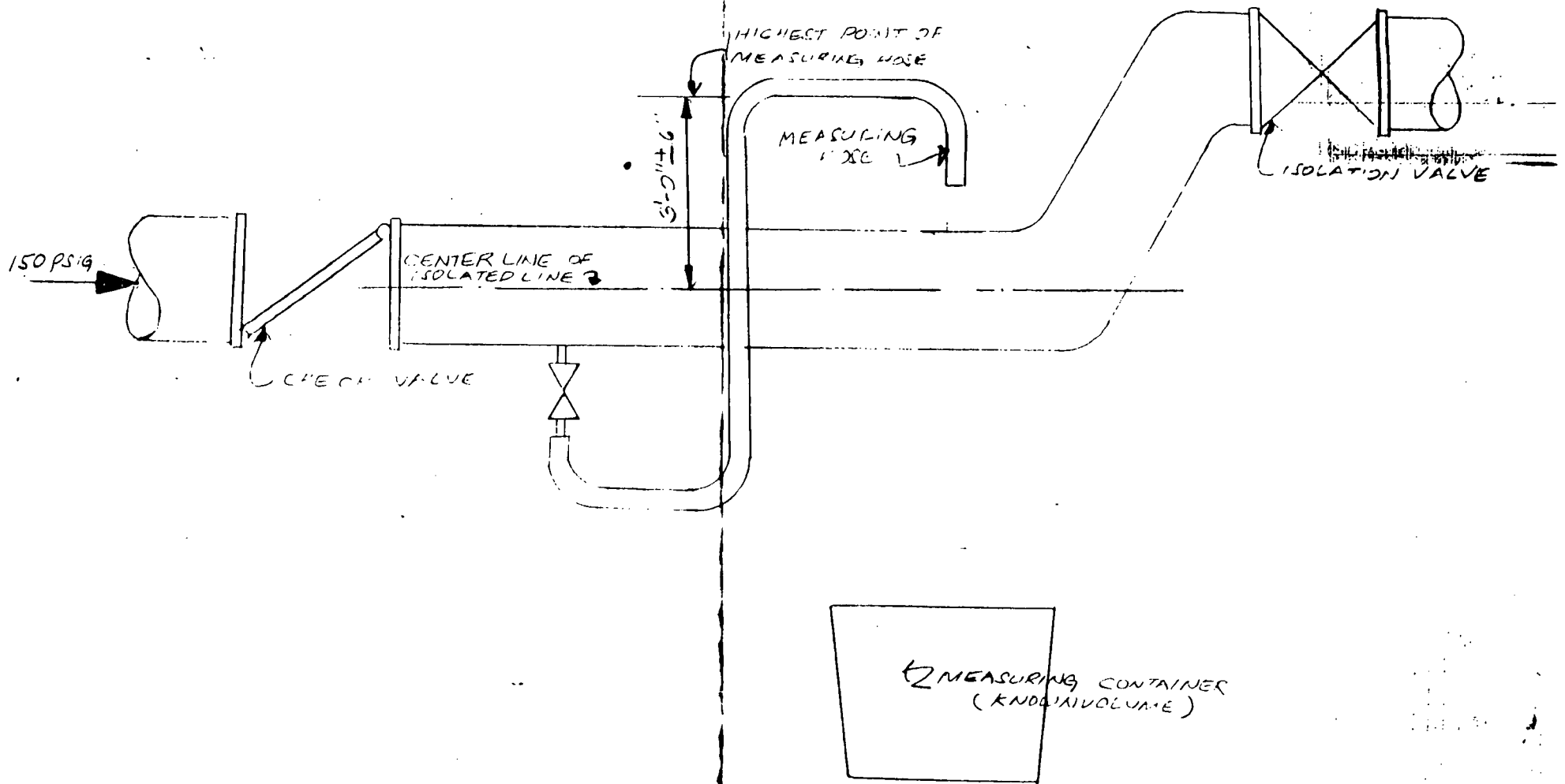
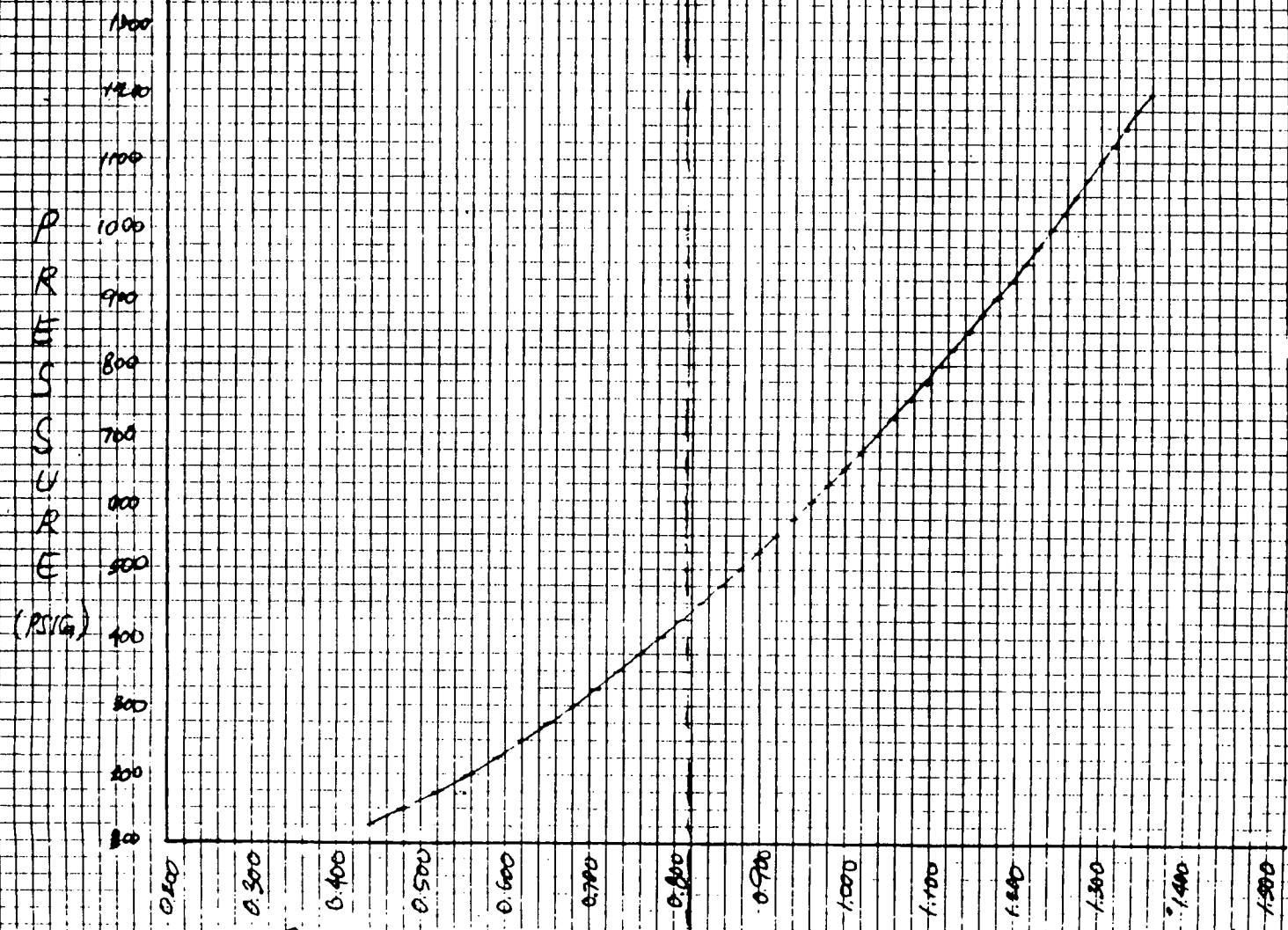


FIG. 1 - TYPICAL HOOKUP OF MEASURING HOSE FOR CHECK VALVE BACKFLOW LEAKAGE TEST.

FIG. 2 - ALLOWABLE CHECK VALVE  
BACK FLOW LEAKAGE RATE



CHECK VALVE BACK FLOW LEAKAGE RATE (GPM)

NOTE: TESTS SHOULD BE PERFORMED AT 150PSIG OR GREATER  
WHENEVER POSSIBLE.



QUESTION NO. 4

Please clarify your commitment with regard to opening and visually inspecting the new check valves. Specifically:

- a. Which valves will be inspected?
- b. How often will they be inspected?
- c. If valves are noisy in operation, will inspection periodicity be increased?

RESPONSE

- a. During the Cycle X refueling outage, one 10" valve inside containment, one 10" valve outside containment (downstream of an FCV), one 12" check valve and one 4" check valve will be opened and inspected.
- b. How often the 10" and 12" valves will be inspected will be determined after evaluating the results of the accelerated wear tests to be performed later this year (see response to Question No. 3 of this Enclosure) and evaluating the results of the inspection performed at the next, Cycle X, refueling outage.
- c. Based on the flow stability tests conducted by Drs. Tullis and Rahmeyer, the valves are expected to perform satisfactorily in the short term (i.e., one to two refueling cycles).

The wear testing program is expected to confirm the suitability of these valves for continued use and will establish appropriate inspection intervals for the remaining plant lifetime. Any noise from the valves during operation is expected to be minimal and similar to what was found during the flow stability tests. See response to Question No. 7 of this Enclosure for further discussion of the points.

QUESTION NO. 5

Since less than 165 gpm through the 10-inch check valves is considered to be severe service by the vendor, what additional actions do you intend to take to assure that operations within this regime (AFW flow) will not unacceptably degrade the valve.

RESPONSE

The flow stability tests performed by Dr. Tullis and Dr. Rahmeyer demonstrated that the valve was totally stable throughout the flow range from 40 gpm through 170 gpm. There was no noise from the valve nor were there any detectable pressure fluctuations downstream of the valve that would be indicative of an unstable disc. The accelerated wear tests to be performed later this year will also encompass these low flows.

QUESTION NO. 6

Please provide the results of the full scale valve testing performed by Dr. Tullis at Utah State University.

RESPONSE

The report on the tests performed by Dr. Tullis has not yet been completed. As soon as it has been finalized, a copy of it will be provided to the NRC. It is expected that this report can be provided on May 5, 1986.

QUESTION NO. 7

How do you intend to monitor the performance of these valves during startup and operation to determine if they are tapping?

RESPONSE

The loudness and rate of any tapping during startup and operation will be observed and evaluated against the results of the testing program.

Data will be obtained by methods similar to those used in the offsite tests: unaided ear, stethoscope and portable accelerometers. It is not intended to have any valves permanently instrumented for continuous monitoring.

It is expected that the valves' performance in service will be bounded by the results of the offsite testing program. If valve tapping as observed in the plant significantly exceeds the test performance results, the testing program will be reevaluated and further offsite testing may be performed.

QUESTION NO. 8

In Table 8 of Appendix D, provide the reason for replacement of the internals to valve DWN309.

RESPONSE

One hundred and forty-one maintenance orders were examined to identify troublesome check valves exhibiting past failures similar to failures seen following the water hammer event.

By reviewing old maintenance records, five check valves were identified and inspected which had problems during the last San Onofre Unit 1 outage, ranging from a history of seat leakage to a cracked diaphragm. The 1986 current inspection results indicated no abnormal wear, no internal or external damage and all are operable.

To be specific, check valve S1-DWN-309 was chosen for inspection because its internal parts were replaced during the last outage. During this current refueling the internals were found to have no wear, no damage and were fully operable. Therefore, the internals were not replaced during this outage and no further action is required.

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ENCLOSURE 3

RESPONSE TO APRIL 29, 1986 LETTER

QUESTION NO. 1

Provide schedules for the implementation of all corrective actions listed in Section 6.5.7.3 of the April 8, 1986 report.

RESPONSE

- a. Prior to return to service from the current outage, the TSC Fox III computer software will be modified to provide for automatic resumption of data collection when power is restored following any loss of power to the computer.
- b. It is our intent to provide an uninterruptible power source (UPS) for the Fox III computer prior to return to service from the current outage. However, since on outage is not required for installation of this modification, if installation is not completed prior to return to service, the installation efforts will continue such that this modification will be implemented no later than July 15, 1986.
- c. Vital bus no. 4 is scheduled to be provided with a UPS during the next refueling outage following return to service from the current outage.

## QUESTION NO. 2

Provide the status and schedule of your efforts to respond to IE Information Notice 84-90, dated December 7, 1984. Will these efforts evaluate the containment pressure response considering the effect of superheat due to tube bundle uncover in steamline break transients?

## RESPONSE

### Outside Containment

The impact of superheated steam blowdown on EQ outside containment is currently being evaluated. Westinghouse is generating plant-specific mass and energy release data similar to data provided to the WOG HELB/SBOC subgroup (WCAP-10961-P). The scheduled delivery of mass and energy data is June 1, 1986. Using the blowdown data developed, Impell Corp. will determine post-accident environmental conditions in the affected areas, assess the environmental qualification of equipment for the superheat profiles, perform equipment thermal response analysis where necessary, and recommend qualification solutions for equipment which is judged to be unqualified. The Impell evaluation and issuance of final report is scheduled to be completed 15 weeks after receipt of the blowdown data.

### Inside Containment

The impact of superheated steam blowdown on EQ inside containment has been evaluated generically by Westinghouse. On January 25, 1985 Westinghouse met with the NRC to provide additional information on an NRC question on WCAP-8822 which is the mass/energy release topical. Westinghouse presented results of analyses performed using the superheat mass/energy release model developed in 1984. The results of these analyses supported the conclusions reached in the August 1983 SER on WCAP-8822 which stated that no reanalysis was required for dry containments. Westinghouse committed to provide a supplement to WCAP-8822 to include the details of the presentation. Supplement 2 to WCAP-8822 (Reference 1) was submitted to the NRC on October 7, 1985. Supplement 2 included the results of a sensitivity study on containment response using the superheat and non-superheat models and concluded that the effects of superheat were negligible. The NRC concurred with Westinghouse that superheat mass/energy does not require reanalysis inside dry containments. NRC concurrence was documented in Reference 2 which concluded that current mass/energy release calculations (without the superheat model) are adequate and revised temperature profiles for environmental qualification of equipment are not required. Based on discussions with Westinghouse, the results of Supplement 2 to WCAP-8822 are applicable to SONGS-1. Containment response analysis for SONGS-1 was submitted to the NRC in References 3 and 4. These analyses used the mass/energy release methodology of WCAP-8822 (without the superheat model).



## References

1. Supplement 2 to WCAP-8822, "Impact of Steam Superheat in Mass/Energy Releases Following a Steamline Rupture For Dry and Subatmospheric Containment Designs" dated September, 1985.
2. Letter from Hugh Thompson to Edward L. Jordan, subject: I&E Information Notice 84-90, dated July 15, 1985
3. Letter from K. P. Baskin (SCE) to D. M. Crutchfield (NRC), Docket 50-206 Automatic Initiation of Auxilliary Feedwater System SONGS-1, dated June 10, 1980.
4. Letter from K. P. Baskin (SCE) to D. M. Crutchfield (NRC), Docket 50-206, Automatic Initiation of Auxilliary Feedwater System SONGS-1, dated March 6, 1986.

QUESTION NO. 3

Submit for staff review the re-analysis of Loss of Normal Feedwater and Main Feedline Rupture transients which are mentioned in Sections 6.1.2.2 and 6.1.2.3 of the April 8, 1986 report.

RESPONSE

See the response to Question No. 9 in Enclosure 1.

QUESTION NO. 4

Spurious indication of safety injection on loss of power.

- a. Is the new power source for the SI annunciator auxiliary relay contact chain "backup up by an" or is it an uninterruptible power supply (UPS)?
- b. Is the new power source the same power source that powers the annunciator? If not, indicate how spurious indication is prevented.
- c. Is the new power source Class 1E and diesel backed?
- d. Describe the power sources for the UPS and their priorities. Is divisional independence maintained?

RESPONSE

- a. The SI annunciator relay auxiliary contact chain will be powered from a UPS through the security UPS distribution system. However, the security UPS will be disconnected and the distribution panel will be powered by the Units 2&3 non-Class 1E UPS.
- b. No - The new power source is used to power the relay coil of the SI alarm relay. A contact from this relay will be used to pick up the annunciator window. The annunciator system power source is the 125 V DC system. This system is powered by the station batteries which are backed up by the diesel generators through the battery chargers. Since both the SI alarm relay and the annunciator system are both battery and diesel generator backed, no spurious SI alarm is postulated.
- c. The UPS and all the associated circuits are non-Class 1E. However, the Units 2 and 3 non-1E UPS is backed up by batteries and diesel generators.
- d. The primary source of power is the Unit 2&3 non-1E UPS inverter which supplies regulated 120 VAC to the system. This inverter is supplied with 125 V DC from non-1E battery system as well as from diesel backed 1E AC source via battery charger. In the event of loss of inverter, a static switch automatically transfers the UPS loads to a non-1E MCC via a regulating transformer.

Note: The SI annunciator relay circuit will be eventually powered from vital bus no. 4 UPS. As stated in our response to Question No. 1 in this Enclosure, this work is planned to be implemented during Cycle X Outage.

QUESTION NO. 5

Spurious remote indication for safeguard load sequencers.

- a. Section 6.2.4.11 indicates that sequencer 1 and a spare logic board were tested. Was sequencer 2 and the plant wiring tested? If not, address the acceptability of not testing this equipment.

RESPONSE

Sequencer 2 was tested using MO 86021238. Testing was completed March 27, 1986. The second sequencer and existing wiring up to the remote panel was tested. Field transmission loops were not tested under this MO since they are included in the normal surveillance program. No defects or abnormalities were found.

QUESTION NO. 6

Reactance bypass circuit breaker.

- a. Will the alarms be both local and in the control room?
- b. Are the alarms actuated on the conditions diesel generator breaker closed and reactance breaker closed, or some other conditions?
- c. When will the operating procedures be modified to incorporate the action to be taken in the event that this alarm sounds?

RESPONSE

- a. No. The "sources parallel" annunciation will be provided only in the Control Room.
- b. Annunciators are actuated under the following conditions:
  - i. Transformer A (B) is paralleled with transformer 'C',
  - ii. Transformer A (B) is paralleled with diesel #1 (#2), or
  - iii. Transformer 'C' is paralleled with diesel #1 (#2) and the reactor bypass breaker RX1 (RY1) is not open.
- c. The procedures will be modified prior to return to service from the current outage (defined as entry into MODE 2).

QUESTION NO. 7

Vital bus 4.

- a. Describe in greater detail the UPS that will be provided as one of the power sources for vital bus 4. Will it be the normal power source? What are its power sources? Is divisional independence maintained?
- b. Is the UPS sized to account for present and future loads?

RESPONSE

- a. The UPS will be a 7.5 kVA inverter that will be connected to a transfer switch. The transfer switch will be connected to vital bus no. 4 and will allow transfer of the bus from the inverter (normal source) to the existing 130 V AC source (alternate source). The inverter will be connected to the generating unit DC Bus 1.

The normal power source to vital bus no. 4 will be the inverter which is connected to DC Bus 1.

The normal power source will be the inverter which will be connected to DC Bus 1. DC Bus 1 is supplied from battery chargers that are connected to buses that can be supplied from the diesel generator sets. The DC Bus 1 can also be supplied power from 125 V DC Battery 1.

The existing divisional independence of vital bus no. 4, the existing 120 V AC source (which will become the alternate source), DC Bus 1, DC Bus 1 battery chargers, and Battery #1, will be maintained.

- b. The 7.5 kVA inverter and transfer switch exceeds present demand on vital bus no. 4, and expected demand of planned future modifications.

#### QUESTION NO. 8

What was the DC overvoltage high potential test values applied for testing 4160 volt cables? Was this test performed as a step voltage test? What was the time limit the final voltage was held on the cable? If the maximum test voltage was used on old cable, how has SCE assured that no further damage has been incurred in the cable?

#### RESPONSE

The DC overvoltage test value used at San Onofre for testing 4160 volt cables of this type is 28 kV for cables expected to remain in-service. Readings are required at 1/2, 1, 2, 5 and 10 minute intervals during the controlled rise DC voltage test (this is a step voltage test). Voltages are held for approximately one minute and allowed to stabilize. The last full test voltage interval is limited to five (5) minutes. Administrative controls prevent testing in excess of approved limits on equipment or cables which will be left in service.

The DC overvoltage test is performed in accordance with Station Procedure S0123-II-11.153 which is derived from the following established industry and SCE standards:

- o The National Electrical Manufacturers Association Standard for Rubber Insulating Power and Control Cables, Publication 49-141, February 1949, (recommends A.C. and D.C. overpotential test levels for cables).
- o The Insulated Power Cable Engineers Association General Specification for Wire and Cable with Rubber, Rubber-like and Thermoplastic Insulation, Second Edition, February 1951, (also recommends A.C. and D.C. overpotential test levels for cable).
- o The Southern California Edison Company Apparatus Division prepared "Instructions and Test Procedure, Over-voltage Testing of Power and Control Cable", dated May 21, 1956, which established A.C. and D.C. test levels based on existing National Standards, including those listed above.
- o The Association of Edison Illuminating Companies, Specification for Ethylene Propylene Rubber Insulated Cables, AEIC 6-73, has been also used as the basis for subsequent revisions to the SCE Test Procedure. It's latest edition is AEIC CS6-82.
- o The present SCE Test Procedure 6A2, last revised June 27, 1983, is included in SCE Substation Test Manual, Section 6A2. This procedure specifies D.C. test voltage levels similar to and consistent with those recommended in the above standards as refined by years of company experience. (S0123-II-11.153 refers to this SCE procedure.)

SCE has utilized DC overvoltage testing at generating stations and substations for over thirty (30) years. When correctly implemented the test will detect imminent cable failures and will not deteriorate the cable. Further, representative samples of 4kV cables that have been in serve at San Onofre Unit 1 since initial operation and were also recently DC overvoltage tested, have subsequently been laboratory tested to breakdown at voltages significantly higher than 28kV DC. Therefore, SCE is assured that no damage was incurred in 4160 volt cables which were DC overvoltage tested.



QUESTION NO. 9

The core ground insulation test indicated one hundredth of a meg-ohm resistance. This resistance is lower than the resistance measured during 1979 test. How do these values compare with previous test and/or factory test values? The core ground insulation value is extremely low. Provide the basis and rationale for accepting this value for safe operation of this transformer.

RESPONSE

The core ground insulation resistance values are as follows:

Factory Test	March 1979	2025 M
Initial Installation	08/01/79	14 K
Latest Test	12/17/85	10 K

During operation, the core is grounded by a ground strap so that the core to ground resistance is essentially zero. To perform this test, this ground strap is removed.

Generally the core voltages are in the region of milli-volts to a few volts. The presence of an additional high resistance ground path may cause extremely small circulating currents which will have negligible effect on the transformer. Dissolved Gas Analysis (DGA) of the transformer oil will show increased percentage of combustibles should a problem occur. To monitor the condition of the auxiliary transformer C Dissolved Gas analysis will be performed every 6 months. In the past this analysis was performed on an as required basis.

At SCE's fossil-fueled El Segundo plant one transformer has been in operation for 30 years. Its core to ground insulation was recently measured at 7 ohms and has been declared acceptable for use.

QUESTION NO. 10

Provide test data for the tests conducted "as found tests" and "as left tests". How do these tests/data compare to the previous years' tests and/or factory tests for transformer C and other equipment tested?

RESPONSE

"As found" and "as left" test data is attached. These tests compare favorably with previous tests conducted by SCE. One exception being the core to ground insulation as explained in the response to Question No. 9 in this Enclosure.

DC overvoltage test data for Safety Related 4 kV cables is also attached.

\* \* \* \* \* PLANNING APPROVALS CONTINUED \* \* \* \* \*

WORK PLANNED	HOGAN, W	12/13/85	08:14:55
WORK PLANNED REVIEW	GLOVER, F	12/13/85	09:33:01
ENGINEERING REVIEW	KHAMAMKAR, S	12/13/85	10:07:41
Q.A. REVIEW	WIMBERLY J	12/13/85	10:42:50
E.C. REVIEW	KUHNS, R	12/13/85	12:05:07
WORK SCHEDULED	KIMMEL, D	12/13/85	12:54:49

\* \* \* \* \* CRAFT INFORMATION \* \* \* \* \*

CRAFT CODE	CRAFT DESCRIPTION	QTY	ESTIMATE HOURS	ACTUAL HOURS
1 - TT	TEST TECHNICIAN	2	16.0	9.6

\* \* \* \* \* MATERIAL REQUIREMENTS \* \* \* \* \*

ESTIMATED DATE OF NEED - / /

--REQ\*N--

NO.	LN	MATERIAL CODE	DESCRIPTION	KEY S	UNIT	QTY	QTY	QTY	LC
				CODE	R	ISS.	RQD	NEEDED	USED

\* \* \* \* \* WORK DONE \* \* \* \* \*

WORK STARTED: DATE - 12/13/85 TIME - 14:00:00

WORK DONE:

12-23-85 PERFORMED CLOSING INSPECTION. NO FOREIGN MATERIALS NOTED. *John P. Amiault*

STEP 2 - 12/13/85 PERFORMED TRANSFORMER TURNS RATIO TEST ON ALL TAPS.

STEP 5 - 12/17/85 PERFORMED TRANSFORMER CORE INSULATION RESISTANCE TEST. 10,000 OHMS

ALTHOUGH READING IS NOT AS HIGH AS IT COULD BE, SHOP SERVICES & INSTRUMENTATION

DIVISION RECOMMENDED TO ACCEPT THE READING, AS THIS CONDITION WILL NOT BE

DETRIMENTAL TO THE OPERATION OF THE TRANSFORMER. *John J. Hopt*

FAULT GAS ANALYSIS

SOUTHERN CALIFORNIA EDISON CO.  
 SHOP & TEST DIVISION  
 501 S. MARENGO AVE.  
 ALHAMBRA, CA 91803

12/17/85  
 1:50 P.M.

ATTN:

LOCATION: SONGS #1  
 BANK & PHASE: "C" BANK AUX  
 SERIAL NUMBER: RCS22281  
 MANUFACTURER: \_\_\_\_\_

VIA PHONE: STEVE

SAMPLE COLLECTED: \_\_\_\_\_  
 SAMPLE ANALYSED: \_\_\_\_\_

PREVIOUS ANALYSIS:  
 PREVIOUS REPORT No.:

SAMPLE VOLUME:  
 GAS VOL. @ 25 C:  
 VOL. % GAS IN OIL:

SAMPLE CONTAINER: \_\_\_\_\_  
 GAS VOLUME @ STP:  
 OIL TEMPERATURE:

COMPONENT

VOL. % IN OIL

HYDROGEN	<u>.0002</u>
OXYGEN	<u>1.2417</u>
CO2	<u>.0331</u>
ETHYLENE	<u>.0004</u>
ETHANE	<u>0</u>
ACETYLENE	<u>0</u>
NITROGEN	<u>9.0776</u>
METHANE	<u>0</u>
CO	<u>.0006</u>
SUMS:	<u>10.36</u>

COMMENTS:

- ALL GASES ARE WITHIN NORMAL LIMITS
- POSSIBLE THERMAL DECOMPOSITION OF CELLULOSE
- POSSIBLE LOW ENERGY SPARK INVOLVING CELLULOSE
- POSSIBLE LOW ENERGY SPARK NOT INVOLVING CELLULOSE
- POSSIBLE SEVERE LOCAL OVERHEATING NOT INVOLVING CELLULOSE

OTHER \_\_\_\_\_

WATER 6 PPM  
 IFT 21 dynes/cm  
 ACID .012 ms KOH/g  
 COLOR NO. .5

P.C.B. \_\_\_\_\_ PPM.

# TRANSFORMER TEST

DATE 12-11-22 T59 NO. 0001-1000

**AS FOUND**

P.O. NO. \_\_\_\_\_

KVA 30,000 MAKE WEST CLASS OR TYPE SL-0A FORM NO. \_\_\_\_\_ SERIAL NO. RCS-2228-1

CYCLES 60 PHASE 3 POLARITY Sub Δ-Δ GALLONS OIL 10046% IMPEDANCE 60 CYC. 11-11-22 (50 CYC.) \_\_\_\_\_

HIGH VOLTAGE 241500 - 235750 - 230000 - 224250 - 218500 LOW VOLTAGE 4360 "X" 4360 "Y"

AMPERES 75.3 77.2 AMPERES 1968.3 1968.3

S.C.E. Co. SPEC. NO. \_\_\_\_\_ WIRING DIAG. ON N.P. \_\_\_\_\_ BLUE PRINT, TEST NO. \_\_\_\_\_

FOR OUTDOOR INSTALLATION. METHOD OF COOLING OA MFR. SPEC. NO. \_\_\_\_\_ M. S. T. No. 2596

## RATIO AND POLARITY

ADJ. POS.	STRAP CONNECTIONS	TTR No. <u>28-7164</u> TEST RATIO						NOMINAL RATIO			POLARITY DIAGRAM
		H1 X1	H2 X2	H1 X1	H3 X3	H2 X2	H3 X3	HV	LV	RATIO	
4	"X" WNDG	51.405	51.390	51.383				224250	4360	51.433	
4	"Y" WNDG	51.406	51.384	51.381				224250	4360	51.433	

## RESISTANCE $K = 1.245$

INIT. R. CRABB

WINDING VOLTAGE <u>22450</u> MAT'L. <u>COPPER</u>				WINDING VOLTAGE <u>4360 x 4360</u> MAT'L. <u>COPPER</u>				
INSTR. NO. <u>52-0503</u> <u>14</u> °C				INSTR. NO. _____ <u>14</u> °C				
CONNECTIONS	READING	K	OHMS	CONNECTIONS	"X" READING	"Y"	K	OHMS
H1 H2	.1783	20	3.566	X1 X2	.0461	.0490	.05	.002305 .002450
H1 H3	.1785	20	3.570	X1 X3	.0462	.0485	.05	.002310 .002425
H2 H3	.1782	20	3.564	X2 X3	.0465	.0487	.05	.002325 .002435
			10.700					.00694 .00731
			x1.5					x1.5 x1.5
			16.050					.01041 .010965

## RESISTANCE CORRECTED TO 75 °C

INIT. \_\_\_\_\_

HIGH VOLTAGE WINDING 19982 (4) OHMS. PHASE AMPS \_\_\_\_\_ I<sup>2</sup>R \_\_\_\_\_  
 LOW VOLTAGE WINDING X = .01296 Y = .01365 OHMS. PHASE AMPS \_\_\_\_\_ I<sup>2</sup>R \_\_\_\_\_

## IMPEDANCE

WINDINGS

INSTR. NO.	<u>52-0506</u>		<u>POLYMER</u>		TEMP. _____ °C	H.V. _____	L.V. _____		
% IMP.	VOLTS	K	AMPS.	K	E/I	WATTS	K	W/I <sup>2</sup>	TEST WATTS @ _____ °C
			SEE ATTACHED SHEET						I <sup>2</sup> R WATTS @ _____ °C
									STRAY WATTS @ _____ °C
									STRAY WATTS @ _____ °C
									I <sup>2</sup> R WATTS @ _____ °C
									IMP. WATTS @ _____ °C

MEGCHAMETER 52-0504

## INSULATION TESTS

INIT. \_\_\_\_\_

X-Y	OIL °C	HIGH TO LOW	HIGH TO GROUND	LOW TO GROUND	CORE TO GROUND (OHMS)	OIL TEST
<u>2800</u>	<u>14</u>	<u>1800 - X</u>	<u>1800</u>	<u>2400 - X</u>	<u>N/A</u>	<u>DOUBLE</u>
		<u>2000 - Y</u>		<u>2400 - Y</u>		

1 MINUTE READINGS } HIGH TO LOW AND GROUND N/A KV. FOR 1 MINUTE. RESULTS \_\_\_\_\_  
 HIGH POTENTIAL TESTS } LOW TO HIGH AND GROUND N/A KV. FOR 1 MINUTE. RESULTS \_\_\_\_\_

## CORE LOSS

INIT. R. CRABB

INSTR. NO.	AM NO.	WM NO.					
VOLTS	K	AMPERES	AVG.	K	WATTS	K	% Exc. CUR.

MAKE WEST

KVA. 30,000

SERIAL NO. RCS 2228-1

	S.C.E. Co. TESTS	MFR. CERTIFIED TEST	MFR. GUARANTEE	REMARKS
CORE LOSS 100% VOLTAGE				
CORE LOSS 110% "				
% EXCITING CURRENT 100% VOLTAGE				
% EXCITING CURRENT 110% "				
H.V. RESISTANCE @ 75 °C <u>TAP 4</u>	<u>19.982</u>			
L.V. RESISTANCE @ 75 °C <u>X</u>	<u>.01296</u>	<u>.01321</u>		
	<u>.01365</u>	<u>.01372</u>		
I <sup>2</sup> R LOSS HIGH VOLTAGE				
I <sup>2</sup> R LOSS LOW VOLTAGE				
WATTS EDDY LOSS				
IMPEDANCE WATTS @ °C				
% IMPEDANCE VOLTS				
% REGULATION 100% P. F. FULL LOAD				
% " 80% " " "				
TOTAL LOSSES				
°C RISE-COPPER-HIGH VOLTAGE WINDING				
°C RISE- " -LOW " "				
NOISE LEVEL (DECIBELS)				

EFFICIENCIES AT 100% P. F.			INSULATION POWER FACTOR								
% LOAD	25	100	H TO L-G			LO TO HI-G			H & LO TO G		
			CAPACITANCE (MF) READ	K=	P.F. (%)	CAPACITANCE (MF) READ	K=	P.F. (%)	CAPACITANCE (MF) READ	K=	P.F. (%)
% CORE LOSS											
% IMPEDANCE LOSS											
% TOTAL LOSS											
% EFF. — S.C.E. TESTS											
% EFF. — MFR.'S CERT. TEST											
% EFF. — MFR.'S GUARANTEE											

NO. OF FANS 0, VAC.-PRESS. RELIEF DEVICE YES, EMERG. PRESS. RELIEF DEVICE YES  
 TYPE OF SEAL: SEALED \_\_\_\_\_ GAS  GAS-OIL \_\_\_\_\_ BREATHER \_\_\_\_\_ CONSERV. \_\_\_\_\_  
 TEMPERATURE IND. \_\_\_\_\_ TESTED \_\_\_\_\_ DRYOUT \_\_\_\_\_  
 TAP SETTING LEFT 227250, BUSHING TYPE: H.V. WEST "0" L.V. WEST  
 TAP CHANGER. HIGH VOLTAGE YES LOW VOLTAGE NO TAP CHGR. CENTERED YES  
 LOAD RATIO CONTROL. HIGH VOLTAGE NO LOW VOLTAGE NO  
 SERIES & PARALLEL STRAPS. HIGH VOLTAGE NO LOW VOLTAGE NO  
 CHECKED FOR OIL LEAKS SHOP GAL. OIL REMOVED NONE  
 MECHANICAL INSPECTION—VALVES & FITTINGS SHOP  
 OIL REMOVED BY SHOP FOR INSPECTION NO VACUUM FILLED NO  
 MARKS AS FOUND TEST

WEIGHTS  
 CORE & COILS 30500 LBS.  
 TANK & FITTINGS 52750 LBS.  
 TANK: OIL 10046 GAL. 75350 LBS.  
 COMP'T: OIL \_\_\_\_\_ GAL. \_\_\_\_\_ LBS.  
 TOTAL WEIGHT 208600 LBS.  
 FROM SONGS #1  
 TO ON SITE  
 TEST J. O. 6061-9358  
 DATE 12-11-85  
 TESTED BY R CRAIG  
 CHECKED R PERC  
 APPROVED \_\_\_\_\_

DOUBLE INSULATION TESTS  
MISCELLANEOUS EQUIPMENT

DOUBLE ENGINEERING COMPANY  
WATER TOWN, MASS  
FORM MIE-ME17K

(SPARE BUSHINGS, INSTRUMENT TRANSFORMERS, ETC)

COMPANY <b>SO CAL EDISON</b>	DATE <b>12-12-85</b>
LOCATION OF TESTS <b>SONGS #1</b>	AIR TEMP. <b>14°C</b> OIL TEMP. <b>—</b>
EQUIPMENT TESTED <b>LIGHTNING ARRESTORS</b>	WEATHER <b>CLEAR</b> % HUM. <b>—</b>
<b>"C" BANK AUX</b>	DATE LAST TEST
<b>WEST CPL 3891A18A01</b>	LAST TEST SHEET NO.

COPIES TO

LINE NO	SERIAL NO	TEST KV	EQUIVALENT 10 KV READINGS						% POWER FACTOR		INSULATION RATING
			AMPERES			WATTS			MEASURED	COR 20°C	
			METER READING	MULTI-PLIER	AMPERES	METER READING	MULTI-PLIER	WATTS			
1	78M9016	10	29	.01	.29	16	.002	.032			
2	78M9020	10	28.5	.01	.285	16	.002	.032			
3	78M9025	10	29	.01	.29	16	.002	.032			
4											
5											
6											
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REMARKS

LEGEND: DOUBLE INSULATION TESTING

BUSHINGS, INSULATORS, ETC	WOOD MEMBERS, ETC, ETC	BINDINGS
SG-GOOD	KG-GOOD	WG-GOOD
D-DETERIORATED	KD-DETERIORATED	WD-DETERIORATED
I-INVESTIGATE	KI-INVESTIGATE	WI-INVESTIGATE
R-HAD REMOVED OR RECONDITIONED	KR-HAD REMOVED OR RECONDITIONED	WR-HAD REMOVED OR RECONDITIONED

OIL  
ASKAREL  
AIR  
GAS

DOUBLE INSULATION TESTS

# THREE - WINDING TRANSFORMER

DOUBLE ENGINEERING COMPANY  
WATERTOWN, MASSACHUSETTS  
MH-JW7701

MO 85120824

COMPANY	So Cal Edison	DIVISION	5513	DATE	12-12-85
LOCATION OF TESTS	SONGS #1	AIR TEMP.	14°C	TOP OIL TEMP	13°C
TRANSFORMER	"C" AUX	WEATHER	CLEAR	% HUMIDITY	N/A
MFR.	WEST	SERIAL NO.	RCS 2228-1	AGE	1979
TYPE/CLASS	OA	KVA	30,000		
FREE BREATHING	<input type="checkbox"/>	SEALED	<input type="checkbox"/>	GAS BLANKETED	<input checked="" type="checkbox"/>
CONSERVATOR	<input type="checkbox"/>	GALLONS OF OIL	10,046		
BUSHINGS	HIGH SIDE KV	230	Y <input type="checkbox"/> Δ <input checked="" type="checkbox"/>	MFR.	WEST
	LOW SIDE KV	4.36	Y <input type="checkbox"/> Δ <input checked="" type="checkbox"/>	TYPE	"O"
	TERTIARY KV	4.36	Y <input type="checkbox"/> Δ <input checked="" type="checkbox"/>	CLASS	90081L
	NEUTRAL			DWG. NO.	273C717ER3
				CAT. NO.	KV
					YEAR
					196
					15
					1979

COPIES TO \_\_\_\_\_ DATE LAST TEST \_\_\_\_\_  
LAST SHEET NO. \_\_\_\_\_

## OVER-ALL TESTS

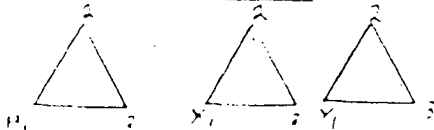
TEST	TEST CONNECTIONS			TEST KV	EQUIVALENT 10KV READINGS						% POWER FACTOR		KEY TO INSULATION RATING G - GOOD D - DETERIORATED I - INVESTIGATE B - BAD (REMOVE OR RECONDITION)	INSULATION RATING
	WINDING ENERGIZED	WINDING GROUNDED	WINDING GUARDED		MILLIAMPERES			WATTS			MEASURED	COR. 20°C		
					METER READING	MULTI-PLIER	MILLI-AMPERES	METER READING	MULTI-PLIER	WATTS				
1	HIGH	LOW	TERT	10	90	.2	18.0	5.0	.1	.50	.278	.278	4748	
2	HIGH		LOW AND TERT.	10	58	.2	11.6	4.0	.1	.40	.345	.345	3048	
3	LOW	TERT.	HIGH	10	78	.2	15.6	7.5	.1	.75	.481	.481	4136	
4	LOW		HIGH AND TERT.	10	75	.2	15.0	7.0	.1	.70	.467	.467	3966	
5	TERT.	HIGH	LOW	10	24	1	24.0	4.5	.2	.90	.375	.375	6270	
6	TERT.		HIGH AND LOW	10	85.5	.2	17.1	7.2	.1	.72	.421	.421	4530	
7	ALL			10	44	1	44.0	9	.2	1.80	.409	.409		
CALCULATED RESULTS							6.4			.10	.156	.156	CL 1 TEST 1 MINUS TEST 21	1670
							.6			.05	.833	.833	CL 1 TEST 3 MINUS TEST 41	170
							6.9			.18	.261	.261	CL 1 TEST 5 MINUS TEST 61	1740

## BUSHING TESTS

LINE NO.	BUSH NO.	PHASE	BUSHING SERIAL NO.	TEST KV	EQUIVALENT 10KV READINGS						% POWER FACTOR		COLLAR TESTS (WATTS/CURRENT)			INSULATION RATING
					METER READING	MULTI-PLIER	MILLI-AMPERES	METER READING	MULTI-PLIER	WATTS	MEASURED	COR. 20°C	CAP	A/P DATA		
														% PF	CAP	
C1 HIGH SIDE	1		3	10	71.5	.02	1.43	7.5	.01	.075	.524	.543	376.8	.44	382	
	2		4	10	72	.02	1.44	7.6	.01	.076	.528	.546	379.8	.43	384	
	3		6	10	72	.02	1.44	8.0	.01	.080	.556	.575	379.8	.44	38T	
	4	N	3	10	20.2	1	20.2	5.0	.2	1.00	.495	.512	5390		5360	
C2 LOW SIDE	5		4	10	20.5	1	20.5	5.0	.2	1.00	.488	.505	5450		5440	
	6		6	10	21	1	21.0	5.5	.2	1.10	.524	.542	5470		5450	
	7															
	8	N														
TERTIARY	9		CHL	10	63	.1	6.3	6	.02	.12	.190	.190	1667			
	10		CHT	10	66	.1	6.6	6.2	.02	.124	.188	.188	1737			
	11		CLT	10	32.5	.02	.65	6.	.01	.06	.923	.923	171.4			
	12	N														
13																
14	OIL SAMPLE			10	87	.01	.87	4	.002	.008	.092	.117	OIL TEMP. 13°C			

N - NEUTRAL

DIAGRAM



REMARKS



# EXCITATION - CURRENT TESTS

## SINGLE PHASE

ENERGIZE	UST
H <sub>1</sub>	H <sub>2</sub> (or H <sub>0</sub> )
H <sub>2</sub> (or H <sub>0</sub> )	H <sub>1</sub>

## THREE-PHASE WYE(1)

ENERGIZE	UST	PHASE
H <sub>1</sub>	H <sub>0</sub>	A
H <sub>2</sub>	H <sub>0</sub>	B
H <sub>3</sub>	H <sub>0</sub>	C

## THREE-PHASE DELTA(1) ✓

ENERGIZE	UST	GROUND	PHASE
H <sub>1</sub>	H <sub>2</sub>	H <sub>3</sub>	A
H <sub>2</sub>	H <sub>3</sub>	H <sub>1</sub>	B
H <sub>3</sub>	H <sub>1</sub>	H <sub>2</sub>	C

## THREE-PHASE AUTO

ENERGIZE	UST	PHASE
H <sub>1</sub>	H <sub>0</sub> X <sub>0</sub>	A
H <sub>2</sub>	H <sub>0</sub> X <sub>0</sub>	B
H <sub>3</sub>	H <sub>0</sub> X <sub>0</sub>	C

MFR. WEST SERIAL NO. RCS - 2228-1

NLTC POSITION (CHECK): 1(A) LINE 2 2(B) \_\_\_\_\_ 3(C) \_\_\_\_\_ 4(D) LINE 1 5(E) \_\_\_\_\_

TAP CHANGER FOUND/LEFT ON POSITION: A - A

TEST VOLTAGE: 10 kV(2)

LINE NO.	(3) ULTC POSITION	MILLIAMPERES									REMARKS
		PHASE A			PHASE B			PHASE C			
		METER READING	MULTIPLIER	MILLIAMPERES	METER READING	MULTIPLIER	MILLIAMPERES	METER READING	MULTIPLIER	MILLIAMPERES	
1		29	.1	2.9	86	.1	8.6	83	.1	8.1	
2		26	.1	2.6	65	.1	6.5	68	.1	6.8	
3											
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**NOTES:**

1. IF THE LOW-VOLTAGE WINDING IS WYE CONNECTED, THEN X<sub>0</sub> IS CONNECTED AS IN SERVICE (USUALLY, THIS WOULD MEAN GROUNDING X<sub>0</sub>)

2. ALL TESTS SHOULD BE PERFORMED ROUTINELY AT THE SAME VOLTAGE:

ENGINEERING DEPARTMENT  
**CALCULATION SHEET**

SUBJECT: C AU 1 XPMR IMPEDANCE DESIGN CALCULATION NO. DC \_\_\_\_\_  
RCS 2228-1 RATED TAP "C"  
 J.O. NO. 6061-9358 MADE BY TZ Cragg DATE 12-17-85 CHK. BY \_\_\_\_\_ DATE \_\_\_\_\_

H1 H2 - X1 X2	E = 486.5	I = .626	∅Z = 11.01
H1 H3 - X1 X3	E = 485.2	I = .632	∅Z = 10.87
H2 H3 - X2 X3	E = 485.8	I = .637	∅Z = 10.91
H2 H5 - X2 Y3	E = 487.0	I = .630	∅Z = 10.95
H1 H3 - Y1 Y3	E = 486.4	I = .630	∅Z = 10.94
H1 H2 - Y1 Y2	E = 486.0	I = .620	∅Z = 11.11

$$\Delta D 18 \text{ } \varnothing Z = \frac{.866 \left( \frac{E_T}{I_T} \times \frac{\text{KVA}}{\text{KV} \times \sqrt{3}} \right) 100}{\text{KV}}$$

TAP 3 KV = 230000  
 KVA = 15000 PER WINDING

POLYMER 520509 DUE 1-5-86  
 RANGE 1.5 AMPS AND 100 VOLTS

*Robert C. Cull*

ENGINEERING DEPARTMENT  
CALCULATION SHEET

SHEET 1 OF 1 SHEETS  
12-11-85  
R. CRABB

SUBJECT: SONGS "C" AUX XPMR DESIGN CALCULATION NO. DC \_\_\_\_\_  
TAP #A IMPEDANCE  
 J.O. NO. 6061-9858 MADE BY \_\_\_\_\_ DATE \_\_\_\_\_ CHK. BY \_\_\_\_\_ DATE \_\_\_\_\_

H <sub>1</sub> H <sub>2</sub> - X <sub>1</sub> X <sub>2</sub>	E = 492.4	I = .665	∅ <sub>0Z</sub> = 11.07
H <sub>1</sub> H <sub>2</sub> - X <sub>1</sub> X <sub>3</sub>	E = 493.6	I = .672	∅ <sub>0Z</sub> = 10.95
H <sub>2</sub> H <sub>2</sub> - X <sub>2</sub> X <sub>3</sub>	E = 492.7	I = .669	∅ <sub>0Z</sub> = 10.98
H <sub>2</sub> - H <sub>3</sub> - Y <sub>2</sub> - Y <sub>3</sub>	E = 490.7	I = .664	∅ <sub>0Z</sub> = 11.02
H <sub>1</sub> H <sub>2</sub> - Y <sub>1</sub> Y <sub>3</sub>	E = 490.1	I = .664	∅ <sub>0Z</sub> = 11.01
H <sub>1</sub> H <sub>2</sub> - Y <sub>1</sub> Y <sub>2</sub>	E = 489.6	I = .653	∅ <sub>0Z</sub> = 11.18

$$\Delta \Delta 18 \phi_{0Z} = \frac{.866 \left( \frac{E I}{K V} \times \frac{KVA}{K V \sqrt{3}} \right)}{K V} 100$$

TAP A KV = 2242.50  
 KVA = 15000 PER WINDING (X-Y)

POLY METER S2-0504 DUE 1-5-86  
 RANGE 1.5 AMPS AND 600 VOLTS

# TRANSFORMER TEST

DATE 12-13-85 T59 No. 6061-9358

P.O. No. \_\_\_\_\_

KVA 30,000 MAKE/TEST SL CLASS OR TYPE SL FORM No. \_\_\_\_\_ SERIAL No. RCS 2228-1  
 CYCLES 60 PHASE 3 POLARITY SUB Δ-Δ-Δ GALLONS OIL 10046% IMPEDANCE 60 CYC. 11-11-20 (50 CYC.) \_\_\_\_\_  
 HIGH VOLTAGE 241500 - 235750 - 230000 - 224250 - 218500 LOW VOLTAGE 4360 'X' 4360 'Y'  
 AMPERES 75.3 AMPERES 1986.3 1986.3  
 S.C.E. Co. SPEC. No. \_\_\_\_\_ WIRING DIAG. ON N.P. \_\_\_\_\_ BLUE PRINT. TEST No. \_\_\_\_\_  
 FOR OUTDOOR INSTALLATION. METHOD OF COOLING \_\_\_\_\_ MFR. SPEC. No. \_\_\_\_\_ M. S. T. No. 2596

## RATIO AND POLARITY

ADJ. POS.	STRAP CONNECTIONS	TTR No. <u>I2 7164</u> TEST RATIO						NOMINAL RATIO			POLARITY DIAGRAM
		H1	H2	H1	H2	H1	H2	HV	LV	RATIO	
		X1	X2	X1	X2	X1	X2				
1	H-X	55.335	55.297	55.272			241500	4360	55.390		
2		54.027	53.990	53.969			235750	4360	54.071		
3		52.683	52.646	52.621			2300000	4360	52.752		
4		51.379	51.343	51.324			224250	4360	51.334		
5		50.075	50.037	50.020			218500	4360	50.115		
1	H-Y	55.328	55.291	55.256			241500	4360	55.390		

$K = 1.266$  RESISTANCE

INIT. RCRABB

WINDING VOLTAGE <u>TAP 1 1/3</u> MAT'L. <u>COPPER</u>						WINDING VOLTAGE _____ MAT'L. _____					
INSTR. NO. <u>S2-0503</u> _____ °C						INSTR. NO. _____ °C					
CONNECTIONS	READING	K	OHMS			CONNECTIONS	READING	K	OHMS		
H <sub>1</sub> H <sub>2</sub>	.1905	.1812	20	3.810	3.624						
H <sub>1</sub> H <sub>3</sub>	.1904	.1811	20	3.808	3.622				SEE TEST		
H <sub>2</sub> H <sub>3</sub>	.1903	.1810	20	3.806	3.620				OF 12-11-85		
				11.424	10.866						
				x1.5	x1.5						
				17.136	16.299						

RESISTANCE CORRECTED TO \_\_\_\_\_ °C

INIT. \_\_\_\_\_

HIGH VOLTAGE WINDING 21.694 20.635 OHMS. PHASE AMPS \_\_\_\_\_ I<sup>2</sup>R \_\_\_\_\_  
 LOW VOLTAGE WINDING \_\_\_\_\_ OHMS. PHASE AMPS \_\_\_\_\_ I<sup>2</sup>R \_\_\_\_\_

## IMPEDANCE

WINDINGS

INSTR. NO.							TEMP. _____ °C	H.V. _____ L.V. _____	
% IMP.	VOLTS	K _____	AMPS.	K _____	E/I	WATTS	K _____	W/I <sup>2</sup>	TEST WATTS @ _____ °C
									I <sup>2</sup> R WATTS @ _____ °C
									STRAY WATTS @ _____ °C
					SEE TEST	OF			STRAY WATTS @ _____ °C
									I <sup>2</sup> R WATTS @ _____ °C
NORMAL									IMP. WATTS @ _____ °C

SEE TEST OF 12-11-85 INSULATION TESTS

INIT. \_\_\_\_\_

OIL °C	HIGH TO LOW	HIGH TO GROUND	LOW TO GROUND	CORE TO GROUND (OHMS)	OIL TEST
FINAL MEGOHMS					
HIGH POTENTIAL TESTS	HIGH TO LOW AND GROUND _____ KV. FOR 1 MINUTE. RESULTS _____				
	LOW TO HIGH AND GROUND _____ KV. FOR 1 MINUTE. RESULTS _____				

## CORE LOSS

INIT. \_\_\_\_\_

AM No. _____	AM No. _____	WM No. _____						
VOLTS	K _____	AMPERES	AVG.	K _____	WATTS	K _____	% EXC. CUR.	

PT. NO. \_\_\_\_\_ CT NO. \_\_\_\_\_ INIT. \_\_\_\_\_

MAKE WESTINGHOUSE

KVA. 30,000

SERIAL NO. RCS 2228-1

	S.C.E. CO. TESTS	MFR. CERTIFIED TEST	MFR. GUARANTEE	REMARKS
CORE LOSS 100% VOLTAGE				
CORE LOSS 110% "				
% EXCITING CURRENT 100% VOLTAGE				
% EXCITING CURRENT 110% "				
H.V. RESISTANCE @ 75 °C 1 5 3	21.694 20.635	20.707		
L.V. RESISTANCE @ °C				
I <sup>2</sup> R LOSS HIGH VOLTAGE				
I <sup>2</sup> R LOSS LOW VOLTAGE				
WATTS EDDY LOSS				
IMPEDANCE WATTS @ °C				
% IMPEDANCE VOLTS				
% REGULATION 100% P.F. FULL LOAD				
% " 80% " " "				
TOTAL LOSSES				
°C RISE-COPPER-HIGH VOLTAGE WINDING				
°C RISE- " -LOW " "				
NOISE LEVEL (DECIBELS)				

EFFICIENCIES AT 100% P.F.			INSULATION POWER FACTOR								
% LOAD	25	100	H TO L-G			LO TO HI-G			H & LO TO G		
			CAPACITANCE (MF) READ	K=	P.F. (%)	CAPACITANCE (MF) READ	K=	P.F. (%)	CAPACITANCE (MF) READ	K=	P.F. (%)
% CORE LOSS											
% IMPEDANCE LOSS											
% TOTAL LOSS											
% EFF. — S.C.E. TESTS			DIRECT								
% EFF. — MFR.'S CERT. TEST			REVERSED								
% EFF. — MFR.'S GUARANTEE			AVERAGE								

NO. OF FANS 0 VAC.-PRESS. RELIEF DEVICE YES EMERG. PRESS. RELIEF DEVICE YES

WEIGHTS INIT. \_\_\_\_\_

TYPE OF SEAL: SEALED \_\_\_\_\_ GAS  GAS-OIL \_\_\_\_\_ BREATHER \_\_\_\_\_ CONSERV. \_\_\_\_\_

TEMPERATURE IND. \_\_\_\_\_ TESTED \_\_\_\_\_ DRYOUT \_\_\_\_\_

TAP SETTING LEFT 4 BUSHING TYPE: H.V. WEST 10" L.V. WEST

TAP CHANGER. HIGH VOLTAGE YES LOW VOLTAGE NO TAP CHGR. CENTERED YES

LOAD RATIO CONTROL. HIGH VOLTAGE NO LOW VOLTAGE NO

SERIES & PARALLEL STRAPS. HIGH VOLTAGE NO LOW VOLTAGE NO

CHECKED FOR OIL LEAKS SHOP GAL. OIL REMOVED NONE

MECHANICAL INSPECTION—VALVES & FITTINGS SHOP

ORE REMOVED BY SHOP FOR INSPECTION NO VACUUM FILLED NO

REMARKS PRIMARY TEST PRIOR TO WORK / INSPECTION

CORE & COILS 80500 LBS.

TANK & FITTINGS 52750 LBS.

TANK: OIL 10046 GAL. 75350 LBS.

COMPT: OIL \_\_\_\_\_ GAL. \_\_\_\_\_ LBS.

TOTAL WEIGHT 20866 LBS.

FROM SONGS #1

TO ON SITE

TEST J. O. 6061-9358

DATE 12-13-85

TESTED BY RCRABB

CHECKED PECK

APPROVED \_\_\_\_\_

Aux C

SOET 30.01

FAULT GAS ANALYSIS

SOUTHERN CALIFORNIA EDISON CO.  
SHOP & TEST DIVISION  
501 S. MARENGO AVE.  
ALHAMBRA, CA 91803

ATTN: ROBERT FECK

LOCATION: ~~3-015~~

BANK & PHASE: 1 WEST TX C AUX.

SERIAL NUMBER: RCS-2228-1 PH.3

MANUFACTURER:

SAMPLE COLLECTED: 29 DEC 85

SAMPLE ANALYSED: ~~17 DEC 85~~

PREVIOUS ANALYSIS: 17 DEC 85

PREVIOUS REPORT No.: 31875

SAMPLE VOLUME: 55.7 ml

GAS VOL. @ 21.5 C: 1.8 ml

VOL. % GAS IN OIL: 4.34 ml

SAMPLE CONTAINER: 179

GAS VOLUME @ STP: 2.42 ml

OIL TEMPERATURE: 17

COMPONENT	PEAK AREA	VOL. % IN OIL	VOL. % IN GAS
HYDROGEN		0.0001	0.0014
OXYGEN	948.0	0.9418	21.6972
CO2	6.5	0.0052	0.1205
ETHYLENE	0.0	0.0000	0.0000
ETHANE	0.0	0.0000	0.0000
ACETYLENE	0.0	0.0000	0.0000
NITROGEN	3590.0	3.3933	78.1739
METHANE	0.2	0.0002	0.0049
CO	0.1	0.0001	0.0021
SUMS:		4.34	100.00

COMMENTS:

ALL GASES ARE WITHIN NORMAL LIMITS

WATER	12	ppm
ACID	41	mg/cm
COLO. NO.	10.5	mg/100ml

**AUX "C"**

**TRANSFORMER TEST** DATE 12-29-85 T59 No. 6061-9358

30000 @ 55° Rise  
 33600 @ 65° Rise West. MAKE West. CLASS OR TYPE SL OA FORM NO. \_\_\_\_\_ P.O. No. \_\_\_\_\_

CYCLES 60 PHASE 3 POLARITY Δ Δ Δ GALLONS OIL 100 % IMPEDANCE 60 CYC. 11.0 (50 CYC.) \_\_\_\_\_

HIGH VOLTAGE 241500 / 235750 / 230000 / 224250 / 218500 LOW VOLTAGE X wdg. 4360 // Y wdg. 4360

AMPERES 71.72 / 73.47 / 75.31 / 77.24 / 79.27 AMPERES 1986.3 @ 15MVA // 1986.3 @ 15MVA

S.C.E. Co. SPEC. No. \_\_\_\_\_ WIRING DIAG. ON N.P. yes BLUE PRINT. TEST No. N.P.

FOR \_\_\_\_\_ INSTALLATION. METHOD OF COOLING OA MFR. SPEC. No. \_\_\_\_\_ M. S. T. No. 2596

**RATIO AND POLARITY**

ADJ. POS.	STRAP CONNECTIONS	TTR No. <u>S2-0503</u> TEST RATIO						NOMINAL RATIO			POLARITY DIAGRAM
		H1 X1	H2 X2	H2 X2	H3 X3	H3 X3	H1 X1	HV	LV	RATIO	
1	H-X	55.351	55.287	55.319				241500	4360	55.390	
2		54.046	53.986	54.010				235750	4360	54.071	
3		52.696	52.639	52.666				230000	4360	52.752	
4		51.394	51.333	51.364				224250	4360	51.433	
5	Y	50.091	50.034	50.060				218500	4360	50.115	
1	H-Y	55.352	55.282	55.314				241500	4360	55.390	

\* Found  $\delta$  left on Tap 4

**RESISTANCE**

WINDING VOLTAGE <u>All HV Taps</u> MAT'L. <u>Cu</u>				WINDING VOLTAGE <u>4360//4360</u> MAT'L. <u>Cu</u>													
INSTR. NO. <u>S2-0503</u> K <u>1.226</u> <u>18</u> °C				INSTR. NO. <u>S2-0503</u> K <u>1.231</u> <u>17</u> °C													
CONNECTIONS	READING			K	OHMS			CONNECTIONS	READING			K	OHMS				
Tap 1	H1-H2	H2-H3	H3-H1		H1-H2	H2-H3	H3-H1	X1-X2					X2-X3				
1	.1961	.1960	.1961	20	3.922	3.920	3.922		.0471		.05	.002355		.0478		.05	.002390
2	.1916	.1912	.1916	20	3.832	3.824	3.832	X3-X1	.0470		.05	.002350	Y1-Y2	.0501		.05	.002505
3	.1868	.1866	.1868	20	3.736	3.732	3.736	Y2-Y3	.0500		.05	.002500	Y3-Y1	.0502		.05	.002510
4	.1821	.1820	.1821	20	3.642	3.640	3.642										
5	.1778	.1775	.1778	20	3.550	3.550	3.550										

RESISTANCE CORRECTED TO 75 °C

HIGH VOLTAGE WINDING (1) 21.6340 (3) 20.6042 OHMS. PHASE AMPS 43.48 I<sup>2</sup>R 38952

LOW VOLTAGE WINDING X .0131009 Y .0138764 OHMS. PHASE AMPS X 1146.8 Y 1146.8 I<sup>2</sup>R 17230 + 18250

**IMPEDANCE**

INSTR. NO.	TEMP. _____ °C						WINDINGS				
	% IMP.	VOLTS	K	AMPS.	K	E/I	WATTS	K	W/I <sup>2</sup>	H.V.	L.V.
										TEST WATTS @ _____ °C	
										I <sup>2</sup> R WATTS @ _____ °C	
										STRAY WATTS @ _____ °C	
										STRAY WATTS @ _____ °C	
										I <sup>2</sup> R WATTS @ <u>75</u> °C <u>74432</u>	
NORMAL										IMP. WATTS @ _____ °C	

No Test

See Test of 12/3/85

**INSULATION TESTS**

S2-0504	OIL °C	HIGH TO LOW		HIGH TO GROUND		LOW TO GROUND		CORE TO GROUND (OHMS)	OIL TEST
		H TO X Y EG RD	X TO Y EG RD	X TO H X EG RD	Y TO H X EG RD	Y TO H X EG RD			
FINAL MEGOHMS	<u>17</u>	<u>3200</u>	<u>3200</u>	<u>1680</u>	<u>1680</u>	<u>1440</u>	<u>1440</u>	<u>No Test</u>	<u>Doble &amp; P.G.A.</u>
HIGH POTENTIAL TESTS		HIGH TO LOW AND GROUND _____ KV. FOR 1 MINUTE. RESULTS <u>NA</u>		HIGH TO GROUND _____ KV. FOR 1 MINUTE. RESULTS <u>NA</u>		LOW TO GROUND _____ KV. FOR 1 MINUTE. RESULTS <u>NA</u>			

**CORE LOSS**

VM NO.	AM NO.	WM NO.					
VOLTS	K	AMPERES	AVG.	K	WATTS	K	% EXC. CUR.
No Test							

MAKE Westinghouse

33600 @ 65° Rise  
KVA. SERIAL NO. RCS-2228-1

	S.C.E. Co. Tests	MFR. CERTIFIED TEST	MFR. GUARANTEE	REMARKS
CORE LOSS 100% VOLTAGE		34116		NA
CORE LOSS 110% "	NA	47879		
% EXCITING CURRENT 100% VOLTAGE		.2792		
% EXCITING CURRENT 110% "		.3220		
H.V. RESISTANCE @ 75 °C	1 21.6340 3 20.6042	③ 20.70703	NA	
L.V. RESISTANCE @ 75 °C	X .0131009 Y .0138764	X .01308 Y .01372		
I'R LOSS HIGH VOLTAGE	38952	39147		
I'R LOSS LOW VOLTAGE	X 17230 Y 18250	17202 18044		
WATTS EDDY LOSS	NA	26706		
IMPEDANCE WATTS @ 75 °C		101099		
% IMPEDANCE VOLTS	See Test of 12-18-85	H-X 10.86 H-Y 11.04 H-X+Y 11.65		
% REGULATION 100% P.F. FULL LOAD		.7760		
% " 80% " " "	NA	7.0907		
TOTAL LOSSES		135215		
°C RISE-COPPER-HIGH VOLTAGE WINDING		51.1		
RISE- " LOW " "		X 61.2 Y 55.7		
RISE LEVEL (DECIBELS)		62.1		

EFFICIENCIES AT 100% P.F.			INSULATION POWER FACTOR					
% LOAD	25	100	H TO L-G		LO TO HI-G		H & LO TO G	
% CORE LOSS	NA		CAPACITANCE (MF)		CAPACITANCE (MF)		CAPACITANCE (MF)	
% IMPEDANCE LOSS			READ	K-	READ	K-	READ	K-
% TOTAL LOSS			See Doble					
% EFF. — S.C.E. TESTS			TEST					
% EFF. — MFR.'S CERT. TEST	99.5065	99.7123						
% EFF. — MFR.'S GUARANTEE								

NO. OF FANS None VAC. PRESS. RELIEF DEVICE yes EMERG. PRESS. RELIEF DEVICE yes

TYPE OF SEAL: SEALED  GAS  GAS-OIL \_\_\_\_\_ BREATHER \_\_\_\_\_ CONSERV \_\_\_\_\_

TEMPERATURE IND. Hez Qualitrol TESTED yes DRYOUT NO

TAP SETTING LEFT 224250 BUSHING TYPE: H.V. Type 0 L.V. Type BT

TAP CHANGER. HIGH VOLTAGE yes LOW VOLTAGE None TAP CHGR. CENTERED OK

LOAD RATIO CONTROL. HIGH VOLTAGE None LOW VOLTAGE None

SERIES & PARALLEL STRAPS. HIGH VOLTAGE None LOW VOLTAGE None

CHECKED FOR OIL LEAKS SSID GAL. OIL REMOVED all

MECHANICAL INSPECTION—VALVES & FITTINGS SSID

REMOVED BY SHOP FOR INSPECTION internal VACUUM FILLED yes

REMARKS Final Test made after internal inspection and filling.

WEIGHTS

CORE & COILS 80500 LBS.

TANK & FITTINGS 52750 LBS.

TANK: OIL 10046 GAL 75350 LBS.

COMPT: OIL \_\_\_\_\_ GAL \_\_\_\_\_ LBS.

TOTAL WEIGHT 20866 LBS.

FROM SONGS 1 "C" Aux.

TO Same

TEST J. O. 6061-9358

DATE 12-29-85

TESTED BY GF./WL

CHECKED \_\_\_\_\_

APPROVED \_\_\_\_\_

Instruments: S2-0503 Bridge cal. due 1-24-86  
S2-0504 Megger Cal. due 1-5-86  
S2-0505 TTR Cal. due 6-24-86



# EXCITATION - CURRENT TESTS

GF/WL

## SINGLE PHASE

<u>ENERGIZE</u>	<u>UST</u>
H <sub>1</sub>	H <sub>2</sub> (or H <sub>0</sub> )
H <sub>2</sub> (or H <sub>0</sub> )	H <sub>1</sub>

## THREE-PHASE WYE(1)

<u>ENERGIZE</u>	<u>UST</u>	<u>PHASE</u>
H <sub>1</sub>	H <sub>0</sub>	A
H <sub>2</sub>	H <sub>0</sub>	B
H <sub>3</sub>	H <sub>0</sub>	C

## THREE-PHASE DELTA(1) ✓

<u>ENERGIZE</u>	<u>UST</u>	<u>GROUND</u>	<u>PHASE</u>
H <sub>1</sub>	H <sub>2</sub>	H <sub>3</sub>	A
H <sub>2</sub>	H <sub>3</sub>	H <sub>1</sub>	B
H <sub>3</sub>	H <sub>1</sub>	H <sub>2</sub>	C

## THREE-PHASE AUTO

<u>ENERGIZE</u>	<u>UST</u>	<u>PHASE</u>
H <sub>1</sub>	H <sub>0</sub> X <sub>0</sub>	A
H <sub>2</sub>	H <sub>0</sub> X <sub>0</sub>	B
H <sub>3</sub>	H <sub>0</sub> X <sub>0</sub>	C

MFR. Westinghouse SERIAL NO. RCS-2228-1  
 NLTC POSITION (CHECK): 1(A)  2(B)  3(C)  4(D)  5(E)   
 TAP CHANGER FOUND/LEFT ON POSITION: 224250/224250  
 TEST VOLTAGE: 10 kv(2)

SONGS Unit 1  
"C" Aux. Bank

LINE NO.	(3) ULTC POSITION	MILLIAMPERES									REMARKS
		PHASE A			PHASE B			PHASE C			
		METER READING	MULTIPLIER	MILLI-AMPERES	METER READING	MULTIPLIER	MILLI-AMPERES	METER READING	MULTIPLIER	MILLI-AMPERES	
1	None	24.2	.1	2.42	43.6	.1	4.36	45.8	.1	4.58	
2											
3											
4											
5											
6											
7											
8											
9											
10											
11											
12											
13											
14											
15											
16											
17											
18											
19											
20											
21											
22											
23											
24											
25											
26											
27											
28											

NOTES:

1. IF THE LOW-VOLTAGE WINDING IS WYE CONNECTED, THEN X<sub>0</sub> IS CONNECTED AS IN SERVICE (USUALLY, THIS WOULD MEAN GROUNDING X<sub>0</sub>).
2. ALL TESTS SHOULD BE PERFORMED ROUTINELY AT THE SAME VOLTAGE.

OIL  
ASKAREL  
AIR  
GAS

DOUBLE INSULATION TESTS

# THREE - WINDING TRANSFORMER

DOBLE ENGINEERING COMPANY  
WATERTOWN, MASSACHUSETTS  
MH-3W7701

COMPANY Southern California Edison DIVISION SSID Alhambra DATE 12-29-85  
 LOCATION OF TESTS SONGS Unit 1 AIR TEMP. 21.5°C TOP OIL TEMP 18°C  
 TRANSFORMER "C" Aux. Bank (Reserve) WEATHER \* See Remarks & HUMIDITY High  
 MFR. West. SERIAL NO. RCS-2228-1 AGE 1979 TYPE/CLASS SL OA KVA 30000 @ 55° Rise  
33600 @ 65° Rise  
 FREE BREATHING  SEALED  GAS BLANKETED  CONSERVATOR  GALLONS OF OIL 10046  
 MFR. TYPE S.O.# DMG. NO. CAT. NO. KV YEAR  
 HIGH SIDE KV 230 Y  Δ  West. O RCS2228 273C717GR3 .196 1979  
 LOW SIDE KV 4.36 Y  Δ  West. XFMR .15 1979  
 TERTIARY KV 4.36 Y  Δ  West. XFMR .15 1979  
 NEUTRAL

COPIES TO \_\_\_\_\_ DATE LAST TEST \_\_\_\_\_  
 LAST SHEET NO. \_\_\_\_\_

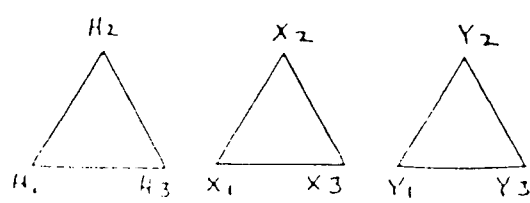
## OVER-ALL TESTS

TEST	TEST CONNECTIONS			TEST KV	EQUIVALENT 10KV READINGS						% POWER FACTOR		KEY TO INSULATION RATING G-6000 D-DETERIORATED I-INVESTIGATE B-BAD (REMOVE OR RECONDITION)	INSULATION RATING
	WINDING ENERGIZED	WINDING GROUNDED	WINDING GUARDED		MILLIAMPERES			WATTS			MEASURED	COR. 20°C		
					METER READING	MULTI-PLIER	MILLI-AMPERES	METER READING	MULTI-PLIER	WATTS				
1	HIGH	LOW	TERT	10	89.5	.2	17.90	4.8	.1	.48	.268	.268	4758 Pfd.	
2	HIGH		LOW AND TERT.	10	58.2	.2	11.64	3.5	.1	.35	.301	.301	3098 Pfd.	
3	LOW	TERT.	HIGH	5	78.25	.2	15.65	12.7	.1	1.27	.812	.812	4160 Pfd.	
4	LOW		HIGH AND TERT.	5	25.2	.2	15.04	12.1	.1	1.21	.805	.805	3988 Pfd.	
5	TERT.	HIGH	LOW	5	23.7	1	2.3.7	5.7	.2	1.14	.481	.481	6275 Pfd.	
6	TERT.		HIGH AND LOW	5	85.7	.2	17.14	9.4	.1	.94	.548	.548	4544 Pfd.	
7	ALL			5	43.85	1	43.85	14.3	.2	2.86	.652	.652	CHECK TEST (SHOULD EQUAL C <sub>1</sub> - C <sub>2</sub> - C <sub>3</sub> ) 11675	
CALCULATED RESULTS							6.26			.13	.208	.208	C <sub>1</sub> (TEST 1 MINUS TEST 2) 1660	
* Measured results below							.61			.06	.984	.984	C <sub>2</sub> (TEST 3 MINUS TEST 4) 172	
							6.56			.20	.305	.305	C <sub>3</sub> (TEST 5 MINUS TEST 6) 173	

## BUSHING TESTS

LINE NO.	BUSHING NO.	P H S E	BUSHING SERIAL NO.	TEST KV	Milli EQUIVALENT 10KV READINGS						% POWER FACTOR		COLLAR TESTS (WATTS/CURRENT)		INSULATION RATING	
					MILLIAMPERES			WATTS			MEASURED	COR. 20°C	TOP	C1		% P.F.
					METER READING	MULTI-PLIER	MILLI-AMPERES	METER READING	MULTI-PLIER	WATTS						
HIGH SIDE	1	H1	3	10	71.65	.02	1.433	7.0	.01	.070	.488	.488	379	382	.44	
	2	H2	4	10	71.6	.02	1.432	6.85	.01	.0685	.478	.478	381	384	.43	
	3	H3	6	10	72.1	.02	1.442	7.2	.01	.072	.499	.499	382	387	.44	
LOW SIDE	4	N														
	5															
	6															
	7															
	8	N														
	9		CHL	10	62.7	.1	6.27	6.95	.02	.139	.222	.222	1666	1666	Pfd.	
	10		CLT	5	65.2	.01	.652	32.4	.002	.0648	.994	.994	172.7	172.7	Pfd.	
	11		CHT	10	65.4	.1	6.54	7.1	.02	.142	.217	.217	173.5	173.5	Pfd.	
	12	N														
	13															
	14		OIL SAMPLE	10	86.2	.01	.862	2.25	.002	.0045	.0522	.0585			OIL TEMP 17 °C K 1.12	

### DIAGRAM



REMARKS: \* Occasional light rain during test.

No Test were made on low voltage or tertiary voltage bushings.

Thermometer I2-9807

DATA RECORD

6.7.3.4 and 6.7.4.3

Date 2-10-86

Rate of Rise: 2 kV/Min Routine Test , Special Test

TIME (Minutes)	A Phase			B Phase			C Phase		
	kV	uA	REMARKS	kV	uA	REMARKS	kV	uA	REMARKS
1/2	9	.1		9	.1		9	.1	
1	9	.1		9	.1		9	.1	
2	11	.1		11	.1		11	.1	
3	13	.1		13	.1		13	.1	
4	15	.1	PI=	15	.1	PI=	15	.1	PI=
5	17	.1		17	.1		17	.1	
6	19	.1		19	.1		19	.1	
7	21	.1		21	.1		21	.1	
8	23	.1		23	.1		23	.1	
9	25	.1		25	.1		25	.1	
10	27	.1		27	.1		27	.1	
11	28	.2		28	.2		28	.1	
12		.1			.1			.1	
13		.1			.1			.1	
14		.1			.1			.1	
15		.1			.1			.1	
22									
23									
24									
25									
26									
27									
28									
29									
30									
31									
32									

MO# 86020871001

CHARGING PUMP 'A'

DATA RECORD

6.7.4 and 6.7.4.3

Date 2-10-86

Rate of Rise: 2 kV/Min Routine Test , Special Test

TIME (Minutes)	A Phase			B Phase			C Phase		
	kV	uA	REMARKS	kV	uA	REMARKS	kV	uA	REMARKS
1/2	9	.1		9	.1		9	.1	
1	9	.1		9	.1		9	.1	
2	11	.1		11	.1		11	.1	
3	13	.1		13	.1		13	.1	
4	15	.1	PI=	15	.1	PI=	15	.1	PI=
5	17	.1		17	.1		17	.1	
6	19	.1		19	.1		19	.1	
7	21	.1		21	.1		21	.1	
8	23	.1		23	.1		23	.1	
9	25	.1		25	.1		25	.1	
10	27	.1		27	.1		27	.1	
11	28	.2		28	.2		28	.1	
12		.1			.1			.1	
13		.1			.1			.1	
14		.1			.1			.1	
15		.1			.1			.1	
22									
23									
24									
25									
26									
27									
28									
29									
30									
31									
32									

NO# 86020871001

CHARGING PUMP B

DATA RECORD

6.7.3.4 and 6.7.4.3

Date 2-26-86

Rate of Rise: 2 kV/Min Routine Test X, Special Test \_\_\_\_\_

TIME (Minutes)	A Phase			B Phase			C Phase		
	kV	uA	REMARKS	kV	uA	REMARKS	kV	uA	REMARKS
1/2	9	.2		9	.1		9	.2	
1	9	.2		9	.1		9	.2	
2	11	.2		11	.1		11	.2	
3	13	.2		13	.1		13	.2	
4	15	.2	PI=	15	.1	PI=	15	.2	PI=
5	17	.2		17	.1		17	.2	
6	19	.2		19	.1		19	.2	
7	21	.2		21	.1		21	.2	
8	23	.2		23	.2		23	.2	
9	25	.2		25	.2		25	.2	
10	27	.2		27	.2		27	.2	
11	28	.2		28	.2		28	.4	
12	2	.2		2	.2		2	.4	
13	2	.2		2	.2		2	.4	
14	2	.2		2	.2		2	.4	
15	2	.2		2	.2		2	.4	
22									
23									
24									
25									
26									
27									
28									
29									
30									
31									
32									

86020868

FEEDWATER PA A

DATA RECORD

6.7.3.4 and 6.7.4.3

Date 2-17-86

Rate of Rise: 2 kV/Min Routine Test , Special Test

TIME (Minutes)	A Phase			B Phase			C Phase		
	kV	uA	REMARKS	kV	uA	REMARKS	kV	uA	REMARKS
1/2	9	1.1		9	6		9	1.5	
1	9	1.2		9	6		9	1.5	
2	11	1.5		11	7		11	1.7	
3	13	1.8		13	9.5		13	1.7	
4	15	3.2	PI=	15	10	PI=	15	1.8	PI=
5	17	3.7		17	12		17	1	
6	19	6		19	20		19	1.6	
7	21	8		21	19		21	1.7	
8	23	6		23	20		23	2.1	
9	25	7		25	32		25	2.4	
10	27	9		27	33		27	2.9	
11	28	13		28	33		28	3.1	
12	28	12		(	30		(	3.2	
13	28	13		(	29		(	3.2	
14	28	13		(	30		(	3.2	
15	28	15		(	30		(	3.2	
22									
23									
24									
25									
26									
27									
28									
29									
30									
31									
32									

MO # 86020851

FEED WATER PP B

DATA RECORD

SST #1

Date 2-22-86

6.7.3.4 and 6.7.4.3

Rate of Rise: 2 kV/Min Routine Test , Special Test

TIME (Minutes)	A Phase			B Phase			C Phase		
	kV	uA	REMARKS	kV	uA	REMARKS	kV	uA	REMARKS
1/2	9	.3							
1	9	.3							
2	11	.3							
5	13	.3							
10	15	.4	PI=			PI=			PI=
11	17	.4							
12	19	.4							
13	21	.5							
14	23	.5							
15	25	.5							
16	27	.6							
17	29	.6							
18		.6							
19		.6							
20		.6							
21		.6							
22									
23									
24									
25									
26									
27									
28									
29									
30									
31									
32									

NOTE: SINCE CABLES ARE SHIELDED TEST WAS MADE W/3 1/2  
CABLES TIED TOGETHER AT EACH END W/SHIELDING  
GROUNDED - *OR*

86020841

DATA RECORD

SST #2

Date 2/05/86

6.7.3.4 and 6.7.4.3

Rate of Rise: 2 kV/Min Routine Test , Special Test

TIME (Minutes)	A Phase			B Phase			C Phase		
	kV	uA	REMARKS	kV	uA	REMARKS	kV	uA	REMARKS
1/2	9	.2		9	.1		9	.2	
1	9	.2		9	.1		9	.2	
2	11	.2		11	.1		11	.2	
3-5	15	.2		15	.1		15	.2	
4-10	15	.2	PI=	15	.1	PI=	15	.2	PI=
5-11	17	.2		17	.2		17	.2	
6-12	19	.2		19	.2		19	.2	
7-13	21	.2		21	.2		21	.2	
8-14	23	.2		23	.2		23	.2	
9-15	25	.2		25	.2		25	.2	
10-16	27	.2		27	.2		27	.2	
11-17	28	.2		28	.2		28	.2	
12-18	2	.2		2	.2		2	.2	
13-19	2	.2		2	.2		2	.2	
14-20	2	.2		2	.2		2	.2	
15-21	2	.2		2	.2		2	.2	
22									
23									
24									
25									
26									
27									
28									
29									
30									
31									
32									

MO # 86020877



SST #3 (NORMAL)

DATA RECORD

6.7.3.4 and 6.7.4.3

Date 5-1-86

Rate of Rise: 2 kV/Min Routine Test X, Special Test \_\_\_\_\_

TIME (Minutes)	A Phase			B Phase			C Phase		
	kV	uA	REMARKS	kV	uA	REMARKS	kV	uA	REMARKS
1/2	9	.2		9	.1		9	.1	
1	9	.2		9	.1		9	.2	
2	11	.2		11	.1		11	.2	
5-3	13	.2		13	.1		13	.3	
10 4	15	.2	PI=	15	.1	PI=	15	.3	PI=
11 5	17	.2		17	.1		17	.3	
12 6	19	.2		19	.1		19	.4	
13 7	21	.2		21	.1		21	.4	
14 8	23	.2		23	.2		23	.4	
15 9	25	.2		25	.2		25	.4	
16 10	27	.2		27	.2		27	.4	
17 11	28	.2		28	.3		28	.4	
18 12	2	.2		2	.3		2	.4	
19 13	2	.2		2	.3		2	.4	
20 14	4	.2		4	.3		4	.4	
21 15	4	.2		4	.3		4	.4	
22									
23									
24									
25									
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27									
28									
29									
30									
31									
32									

MO # 86020840

DATA RECORD

6.7.3.4 and 6.7.4.3 *SST #3 (Alternate).x08* Date 3-1-86  
 Rate of Rise: 2 kV/Mfn Routine Test X Special Test \_\_\_\_\_

TIME (Minutes)	A Phase			B Phase			C Phase		
	kV	uA	REMARKS	kV	uA	REMARKS	kV	uA	REMARKS
1/2	9	.3		9	.1		9	.2	
1	9	.3		9	.1		9	.2	
2	11	.2		11	.1		11	.2	
5 5	13	.2		13	.1		13	.2	
10 4	15	.2	PI=	15	.2	PI=	15	.2	PI=
11 5	17	.2		17	.2		17	.2	
12 6	19	.2		19	.2		19	.2	
13 7	21	.2		21	.2		21	.2	
14 8	23	.2		23	.2		23	.2	
15 9	25	.2		25	.2		25	.2	
16 10	27	.3		27	.2		27	.2	
17 11	28	.3		28	.2		28	.2	
18 12	7	.3		7	.2		7	.2	
19 13	7	.3		7	.2		7	.2	
20 14	7	.3		7	.2		7	.2	
21 15	7	.3		7	.2		7	.2	
22									
23									
24									
25									
26									
27									
28									
29									
30									
31									
32									

MO # 86020878

MO # 86020836

DATA RECORD

DG # 1

6.7.3.4 and 6.7.4.3

Date 2-11-86

Rate of Rise: 2 kV/Min Routine Test , Special Test

TIME (Minutes)	A-B-C $\phi$ 's A Phase <del>2-11</del>			B Phase			C Phase		
	kV	uA	REMARKS	kV	uA	REMARKS	kV	uA	REMARKS
1/2	9	.001							
1	9	.001							
2	11	.001							
5 3	13	.04							
10 4	15	.04	PI=			PI=			PI=
11 5	17	.04							
12 6	19	.04							
13 7	21	.04							
14 8	23	.04							
15 9	25	.05							
16 10	27	.05							
17 11	29	.03							
18 12	29	.03							
19 13	29	.03							
20 14	29	.03							
21 15	29	.03							
22									
23									
24									
25									
26									
27									
28									
29									
30									
31									
32									

NOTE: TEST MADE W/12 1/2 CABLES TIED TOGETHER IN 4KV CABINET 11C14.

BRIDGE READINGS SHIELD TO GROUND.

CONDUIT # 1, A  $\phi$  1.168  $\Omega$  B  $\phi$  1.078  $\Omega$  C  $\phi$  1.072  $\Omega$

" 2. A  $\phi$  1.215  $\Omega$  B  $\phi$  1.263  $\Omega$  C  $\phi$  1.269  $\Omega$

" 3. A  $\phi$  1.056  $\Omega$  B  $\phi$  1.246  $\Omega$  C  $\phi$  1.098  $\Omega$

" 4. A  $\phi$  1.166  $\Omega$  B  $\phi$  1.027  $\Omega$  C  $\phi$  1.019  $\Omega$

AKVR  
TO J.E  
# 717F  
IN DG # 1

DATA RECORD

DG#2

0882

MO# 8602 ~~8820~~

6.7.3.4 and 6.7.4.3

Date 3-5-86

Rate of Rise: 2 kV/Min Routine Test X Special Test \_\_\_\_\_

4KV RMI TO JUNCTION BOX PB9316.

GENERATOR TO JUNCTION BOX

TIME (Minutes)	A B C Phase			B Phase			A B C Phase		
	kV	uA	REMARKS	kV	uA	REMARKS	kV	uA	REMARKS
1/2	9	50.					9	1.5	
1	9	50.					9	1.5	
2	11	50.					11	1.7	
5.3	13	50.					13	2.5	
10.4	15	50.	PI=			PI=	15	3.7	PI=
11.5	17	50.					17	4.2	
12.6	19	50.					19	7.0	
13.2	21	50.					21	7.0	
14.8	25	50.					23	9.0	
15.9	25	50.					25	12.	
16.10	27	50.					27	14.	
17.11	29	50.					29	15.	
18.12		30.						19.	
19.13		30.						20.	
20.14		30.						20.	
21.15		30.						20.	
22									
23									
24									
25									
26									
27									
28									
29									
30									
31									
32									

BRIDGE READINGS

CABLE #1. A. 1.408 Ω B. 1.345 Ω C. 1.311 Ω  
 CABLE #2. A. 1.380 B. 1.238 C. 1.405  
 CABLE #3. A. 1.220 B. 1.374 C. 1.356  
 CABLE #4. A. 1.394 B. 1.385 C. 1.280  
 } 4KV ROOM  
 } TO JUNCTION  
 } BOX

CABLE #1. A. .053 Ω B. .050 Ω C. .051 Ω JUNCTION BOX  
 CABLE #2. A. .052 Ω B. .053 Ω C. .055 Ω TO GENERATOR  
 CABLE #2. A. .052 Ω B. .051 Ω C. .048 Ω

DATA RECORD

SIPUMP 650 A

Date 2-26-86

6.7.3.4 and 6.7.4.3

Rate of Rise: 2 kV/Min Routine Test ✓, Special Test \_\_\_\_\_

TIME (Minutes)	A Phase			B Phase			C Phase		
	kV	uA	REMARKS	kV	uA	REMARKS	kV	uA	REMARKS
1/2	9	.2		9	.1		9	.2	
1	9	.2		9	.2		9	.2	
2	11	.2		11	.2		11	.2	
5	13	.2		13	.2		13	.2	
10	15	.2	PI=	15	.2	PI=	15	.2	PI=
11	17	.2		17	.2		17	.2	
12	19	.2		19	.2		19	.2	
13	21	.2		21	.2		21	.2	
14	23	.3		23	.2		23	.2	
15	25	.3		25	.2		25	.2	
16	27	.3		27	.2		27	.2	
17	28	.3		28	.2		28	.2	
18	7	.3		7	.2		7	.2	
19	13	.3		13	.2		13	.2	
20	14	.3		14	.2		14	.2	
21	15	.3		15	.2		15	.2	
22									
23									
24									
25									
26									
27									
28									
29									
30									
31									
32									

M.O. # 86020869

DATA RECORD

6.7.3.4 and 6.7.4.3

S.I. PUMP GSOB'

Date 2-26-86

Rate of Rise: 2 kV/Min Routine Test , Special Test

TIME (Minutes)	A Phase			B Phase			C Phase		
	kV	uA	REMARKS	kV	uA	REMARKS	kV	uA	REMARKS
1/2	9	.2		9	.2		9	.2	
1	9	.2		9	.2		9	.2	
2	11	.2		11	.2		11	.2	
5	13	.2		13	.2		13	.2	
10	15	.2	PI=	15	.2	PI=	15	.2	PI=
11	17	.2		17	.2		17	.2	
12	19	.2		19	.2		19	.2	
13	21	.2		21	.2		21	.2	
14	23	.2		23	.2		23	.2	
15	25	.2		25	.2		25	.2	
16	27	.2		27	.2		27	.2	
17	28	.2		28	.2		28	.2	
18	)	.2		)	.2		)	.2	
19	)	.2		)	.2		)	.2	
20	)	.2		)	.2		)	.2	
21	Y	.2		Y	.2		Y	.2	
22									
23									
24									
25									
26									
27									
28									
29									
30									
31									
32									

MO # 8602 0848

QUESTION NO. 11

What type of 4160V cable was used for replacement of old cable? Provide information on cable type and materials. What type of testing was performed on the new cable before it is energized?

RESPONSE

The A, B and C transformer replacement feeder cable is 5kV shielded 3 conductor copper 750 or 500 kcmil, with Kerite HTR insulation, aluminum interlocked armor, and a flame-retardant jacket manufactured by Kerite Company (Nos. E1795 and E2058) meeting IEEE 383 (Vertical Tray Flame Test).

The charging pump replacement cable is Anaconda, 8kV shielded 3 conductor copper, 250 kcmil, with ethylene propylene insulation, and a shielded hypalon jacket meeting IEEE 383 (Vertical Tray Flame Test).

All replacement cable is DC overvoltage tested at 36kV in accordance with Station Procedure S0123-II-11.153 prior to being placed in service (in addition to the extensive in-process and product testing conducted by the manufacturers).

QUESTION NO. 12

Provide information on the systematic method for monitoring selected electrical circuits for establishment of a surveillance program as noted in your report, (i.e. EG&G ECCAD system). Does SCE company have in place any other testing program for monitoring cable (and other electrical equipment) integrity over time?

RESPONSE

The method for monitoring selected electrical circuits as described in the April 8, 1986 report utilizes the Electrical Circuit Characterization and Diagnostic (ECCAD) system. The ECCAD System was developed by EG&G Idaho for performing in-situ testing of circuits and is based on an extension of Time Domain Reflectometry (TDR) technology. By inputting a series of short low-voltage pulses into a circuit, ECCAD measures the characteristics of the reflected signal(s) due to impedances in the circuit. The reflected wave forms can be plotted and analyzed for an indication of a circuit's integrity. By comparing baseline plots to subsequent plots, an indication of circuit degradation over time can be interpreted.

SCE has undertaken an effort to acquire a set of baseline plots for selected electric circuits during the current outage. This sample set includes selected instrumentation, 480V, and 4kV circuits. This is being performed as a research and development effort at this time to assess whether or not the TDR technology can produce consistent data that would give an indication of long term circuit condition.

If, as future plots are obtained and analyzed, it is determined that the collected data is credible and meaningful, the usefulness of a long-term surveillance program will be assessed and implemented as appropriate. A systematic selection of a larger sample set will also be evaluated at that time.

SCE Company's testing program for monitoring integrity of electrical equipment is as follows:

1) Cables

H1 Pot tested every 15-20 years. For suspect cables H1 Pot testing is done every 5-10 years.

2) Motors

4 kV - Bridged, Meggared, H1 Potted and impedance tested every refueling (18 months).

480 V - Meggar tested every 12-18 months, overhaul - 5 years, 1st motors every 18 months.



- 3) Buses  
Meggar tested every 36 months.
- 4) Relays  
Functionally tested, calibrated and adjusted every 36-48 months.
- 5) Transformers  
Overhauled every 5 years.
- 6) Turbine Generator  
Inspect, Meggar, Hi Pot, repair every 36 months.
- 7) Breakers  
Inspect test, adjust and replace worn parts every 36 months.

QUESTION NO. 13

It is referenced in section 6.2.1.4 item 6 (page 6-102) that additional design changes are being made to enhance the performance of the electrical system. Item E refers to plant improvement to increase reliability of the electrical system, a modification will be implemented to enhance the availability of the second source of offsite power. Describe what this modification will consist of and when will it be implemented.

RESPONSE

The different options being considered to enhance the availability of the offsite power supply are at present in the developmental stage. Since any improvements in this area cannot be implemented until the next refueling outage, the schedule for completion of the preliminary assessment of the different options, extends into the post-RTS time frame. In addition, due to the significant nature of these types of modifications, their impact on the Integrated Living Schedule at San Onofre Unit 1 is also being evaluated. It is expected that additional information on this subject can be provided to the NRC by June 30, 1986.

QUESTION NO. 14

Has any evaluation and analysis performed to trend the test results to assess the auxiliary transformer C condition and reliability? Provide information, if any, in this regard.

RESPONSE

The test data from 1979/1980 and 1985 were reviewed and found to be comparable.

This review of the test data shows that the auxiliary transformer C is in a condition to operate reliably until the next normal test is performed in 1990. No trending was necessary in the review process.

QUESTION NO. 15

Provide the test voltage value at which the insulation resistance tests were performed for transformer C and other electrical equipment.

RESPONSE

The insulation resistance tests on the auxiliary transformer C were performed at 1000 V DC. Equipment with operating voltage of 480 V and below is tested with 500 V meggar. All others are tested with 1000 V meggar.

QUESTION NO. 16

Would the "4160 volt bus sources parallel" annunciator with 10 second time delay include the diesel generator source when it is paralleled with the offsite source?

RESPONSE

Yes. See answer to Question 6b.

QUESTION NO. 17

Is there any operating mode when diesel generator may be paralleled with auxiliary transformer A and/or B? Is this mode of operations acceptable and would it be covered in the proposed new procedures.

RESPONSE

Yes, for short periods of time, when transferring 4 kV sources. This mode of operations will be covered in revisions to operating procedures to be implemented prior to return to service from the current outage (defined as entry into MODE 2).

QUESTION NO. 18

On page 8-2, item 6, "Guidance will be issued to address the reenergization of station auxiliary equipment using diesel generators....". When will this guidance be issued and/or submitted for NRC review?

RESPONSE

The guidance will be issued prior to return to service from this outage (defined as entry into MODE 2). However, there are no plans to submit this information to the NRC for review.

QUESTION NO. 19

On page 8-3, reference is made to the evaluation of the material condition of electrical power cable to identify causes of the cable failure. When will this evaluation be submitted to NRC? How will the result of this report be incorporated in the evaluation of the remaining cable and/or how the impact of this evaluation of existing cable, if any, be handled by SCE?

RESPONSE

As discussed in Section 6.2.1.3.1, a special Cable Evaluation Task Force was established to conduct an extensive effort to assess the material condition of cable remaining in place. The Task Force is comprised of senior SCE engineers, SCE cable experts, an independent cable consultant and senior Architectural/Engineer personnel. The objective of the Task Force is to determine the mechanisms of failure of both the in-service 4kV C transformer cable fault and the cable failing DC Overvoltage testing, and identify the implications of those failures to other cables.

The Task Force has also removed samples of 4kV cable representative of cable remaining in-service and forwarded those samples to independent laboratories for both physical analysis and electrical testing. The data from these laboratories will be used to establish the material condition of the 4kV cable not replaced. Additionally, by determining the root cause of the above mentioned cable failures, SCE can identify and implement the necessary modifications required to preclude cable failures due to similar causes.

Laboratory results received to date indicate that the cause of the failure of the 4kV cable that initiated the November 1985 transient is directly related to overheating of the cable due to long-term exposure to a localized heat source. SCE has initiated plant walkdowns to identify and eliminate any instances wherein a localized heat source (that could potentially degrade cables) is in direct proximity to cable raceways. Additionally, preliminary results from other laboratory physical analysis and electrical testing confirm that the cable remaining in use at San Onofre Unit 1 has retained its dielectric properties, is suitable for continued use, and has substantive remaining life.

All of the actions, analysis, testing, conclusions and recommendations of the Cable Evaluation Task Force will be documented in a final comprehensive report which will address mechanisms of failure and the material condition of the remaining cable. It is expected that a report will be provided to the NRC by May 30, 1986.



QUESTION NO. 20

The LOVATS and end of sequence light - Is this light a single light and if so, how will its reliability be affected?

RESPONSE

The LOVATS end of sequence light is a single light module with two lamps. Therefore, indication will be maintained even if one lamp burns out. In the event both lamps are out, the operator can verify the end of sequence by observing the status of indicating lights for breakers 11A04 and 11B04. We are not aware of any unexplained failure modes associated with LOVATS end of sequence light like that experienced with the spurious safety injection indication from the safeguards load sequencer neon lamps.

QUESTION NO. 21

For Piping Inside Containment on Feedwater Line B.

- a. Did the licensee ultrasonically inspect each weld that was not replaced?
- b. Will the licensee ultrasonically inspect each weld in the replacement line and the welds connecting the replacement line to the existing line?
- c. Will the licensee radiographically inspect the welds connecting the replacement line to the existing line?
- d. Identify ASME Code and Addenda standard, including class, used to inspect these welds.
- e. Why are indications in piping attached to steam generator E-1B feedwater nozzle considered non-relevant?
- f. Indicate size (length and depth) of flaw remaining in containment penetration C-3C.

RESPONSE

- a. Yes. Each weld that was not replaced was examined by ultrasonic testing (UT).
- b. Yes. Each weld in the replacement line and the welds connecting the replacement line to the existing line were examined by UT. In addition, the surface of the above welds was examined by MT.
- c. No. Radiographic examination is not required by the construction code (see response 21.d for construction code). However, the closure welds connecting the pipe spool to the existing line near the second elbow upstream of the feedwater nozzle on the steam generator will be radiographed.
- d. Replacements were performed in accordance with ASME Section XI, 1977 Edition, with Addenda up through Summer 1978. As permitted by Article IWA-7200 of ASME Section XI, a later edition of the original construction code was used for materials, design, fabrication and installation for replaced piping. The construction code used is ASME Section I, 1983 Edition, which in turn refers to ANSI B31.1, 1980 Edition, including Summer 1980 Addendum, for materials, design fabrication and installation. The construction code required visual examination for the 10 in., 0.500 in. wall pipe welds.

In accordance with the preservice examination requirements, the welds were examined by MT and UT to meet the requirements of ASME Section XI, 1974 Edition, with addenda up through Summer 1975. Since the applicable edition with addenda of ASME Section XI does not have acceptance standards for examination of piping, the provisions in IWB-3514 of ASME Section XI, 1977 Edition, with Addenda up through Summer 1978, was used.

The ISI classification for the feedwater piping inside containment is Class 2.

- e. The UT indications detected in steam generator E-1B feedwater nozzle weld 392-13 (refer to page 6-124, second paragraph) were recorded at an amplitude of 80% DAC. These indications are considered recordable to the applicable ASME Section XI code, but do not require sizing (length and through wall dimensions) or evaluation (a/l aspect ratio) for acceptability (a/t %). The dimensions, a, l and t are defined in Article IWA-3000. Furthermore, since the UT indications exhibited characteristics typical of weld discontinuities and these discontinuities were observed on radiographs taken in 1980, they were determined to be preexisting relative to the event.
- f. The description of three (3) indications remaining in containment penetration C-3C as a result of examination by MT is as follows:
  - o Fillet weld between reinforcing pad and sphere inside containment - Refer to Figure 1 of Attachment 1 for location of indications. One (1) indication, 7/32 in. long, at location B; and one (1) indication, 5/32 in. long, at location C.
  - o Weld between plate and sleeve outside containment - Refer to Figure 2 of Attachment 2 for location of indication. One (1) indication, 1/8 in. long, at location 2.
  - o The indications meet the acceptance criteria of Article IWB-3510.1 (d) of ASME Section XI, 1977 Edition, with Addenda up through Summer 1978.
  - o Due to the configuration of the welds, depth measurement using UT was not feasible.

Also provided as Attachment 2 is a copy of the report that documents the metallurgical and failure analysis for the feedwater piping that was requested in a telephone call with the NRC staff on April 22, 1986.

WESTINGHOUSE NUCLEAR SERVICE DIVISION  
INSPECTION SERVICES

GENERAL - INDICATION DATA

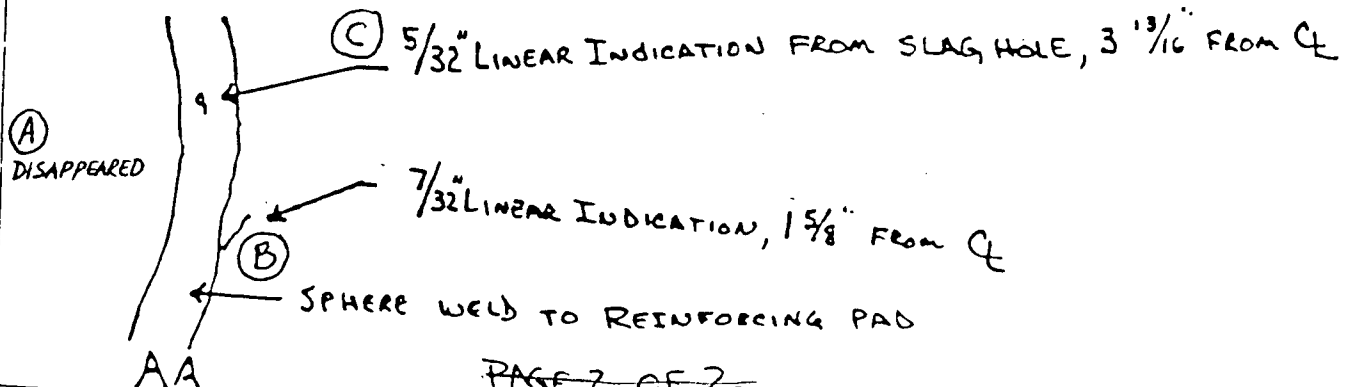
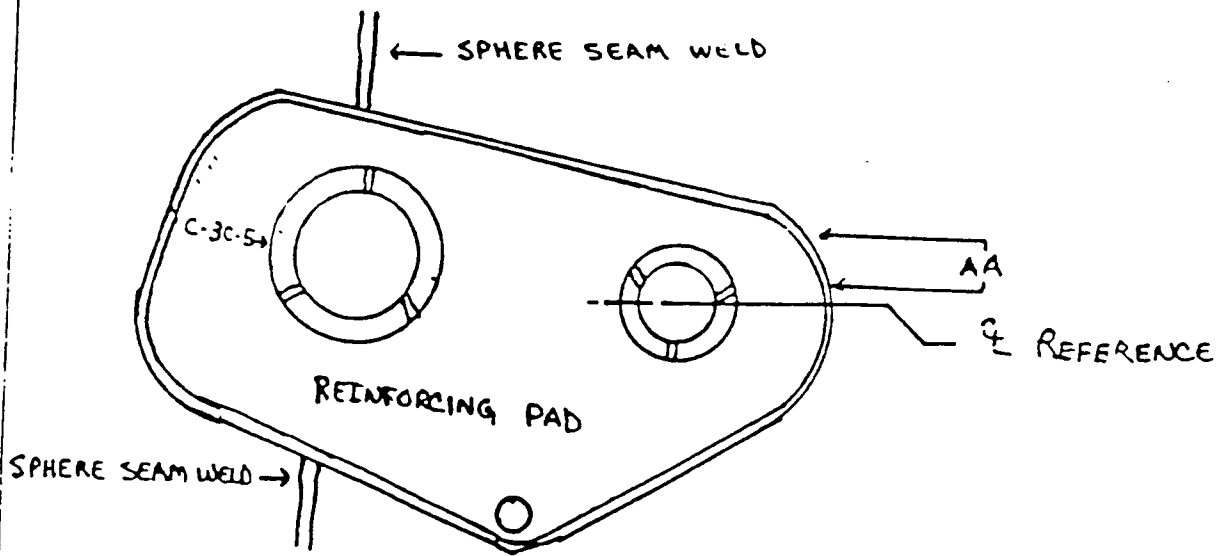
PLANT SAN ONOFRE UNIT 1 SKETCH N/A  
 SYST/COMP CONTAINMENT VESSEL PENETRATION C-3C PROCEDURE 501-W-ISE-70/0  
 EXAMINER James R. Dellursey II DATE 1-17-86  
 LEVEL II

DETECTED BY U/T \_\_\_\_\_ P/T \_\_\_\_\_ M/T  V/T \_\_\_\_\_ IDENT NO. SPHERE WELD TO REINFORCING PAD AT PENETRATION C-3C

PROVIDE SUFFICIENT INFORMATION TO DESCRIBE SIZE, LOCATION AND TYPE OF INDICATION DESCRIBE EXTRA OR SPECIAL EQUIPMENT IF USED FOR SIZING OR REPORTING. IF NECESSARY INCLUDE SKETCH SHOWING GENERAL CONFIGURATION OF ITEM OR AREA.

INSIDE CONTAINMENT

AFTER BUFFING

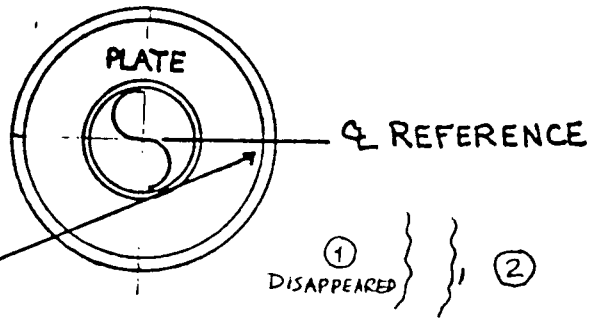


AFTER BUFFING

1-18-86

PENETRATION C-3C OUTSIDE CONTAINMENT

WELD C-3C-1  
PLATE TO SLEEVE WELD



② 1/8" LINEAR INDICATION, TOE OF WELD, SLEEVE SIDE,  
PARALLEL TO WELD, 2 1/8" DOWN FROM C REFERENCE

James R. Dellbusso  
LEVEL II