



QSA GLOBAL

QSA Global, Inc.
40 North Avenue
Burlington, MA 01803
Telephone: (781) 272-2000
Toll Free: (800) 815-1383
Facsimile: (781) 273-2216

25 August 2010

Mr. Pierre Saverot
Division of Spent Fuel Storage and Transportation
Office of Nuclear Material Safety and Safeguards
U.S. Nuclear Regulatory Commission
11555 Rockville Pike, Mailstop: EBB-3D-02M
One White Flint
Rockville, MD 20852

RE: Pending Renewal for USA/9269/B(U)-96 (Current Revision 5)

Dear Mr. Saverot:

Enclosed please find page 3-6 of the 650L SAR Revision 8. This page corrects typographical errors in the equations for H_{os} and Q_{os} as identified in your email dated 24 August 2010. Also enclosed is a copy of the updated List of Affected Pages for the SAR. There are no other changes to the submission/approval at this time. Should you have any additional questions or wish to discuss this submission after receipt please feel free to contact me.

Sincerely,

Lori Podolak
Senior Regulatory Affairs Specialist
Regulatory Affairs Department
Ph: (781) 505-8241
Fax: (781) 359-9191
Email: Lori.Podolak@qsa-global.com

Enclosures:

- SAR List of Affected Pages
- Page 3-6 or Revision 8 to the SAR

Safety Analysis Report for the Model 650L Transport Package

QSA Global Inc.
Burlington, Massachusetts

August 2010 – Revision 8
Page 3-6

$$Q_{LS} = H_{LS} A_{LS} (T_W - T_A)$$

Where $A_{LS} = 0.118 \text{ m}^2$ (total surface area of lid sides) and
 H_{LS} = the free convection coefficient for a vertical surface.

For a heated plate, the free convection coefficient for laminar flow is:

$$H_{LS} = [0.68 + 0.67[(g \beta (T_W - T_A) L^3) / (\nu \alpha)]^{0.25} / \{1 + (0.492 \alpha/\nu)^{9/16}\}^{4/9}] \text{ (K / L)}$$

(Reference: Fundamentals of Heat and Mass Transfer, F.P. Incropera, 4th Edition, 1996, Ch. 9)

Where: $L = 0.056 \text{ m}$ (area/perimeter). Therefore:

$$H_{LS} = 0.346 + 2.67 (T_W - 38)^{0.25}$$

Substituting this into the convection equation for the lid side surface produces:

$$Q_{LS} = 0.041 (T_W - 38) + 0.315 (T_W - 38)^{1.25}$$

Outer shell surface convection (Q_{OS}):

$$Q_{OS} = H_{OS} A_{OS} (T_W - T_A)$$

Where $A_{OS} = 0.124 \text{ m}^2$ (total surface area of the outer shell) and
 H_{OS} = the free convection coefficient for a vertical surface.

For a vertical plate the free convection coefficient for laminar flow is:

$$H_{OS} = [0.68 + 0.67[(g \beta (T_W - T_A) L^3) / (\nu \alpha)]^{0.25} / \{1 + (0.492 \alpha/\nu)^{9/16}\}^{4/9}] \text{ (K / L)}$$

(Reference: Fundamentals of Heat and Mass Transfer, F.P. Incropera, 4th Edition, 1996, Ch. 9)

Where $L = 0.077 \text{ m}$ (area/perimeter). Therefore:

$$H_{OS} = 0.194 + 2.47 (T_W - 38)^{0.25}$$

Substituting and solving for Q_{OS} produces

$$Q_{OS} = 0.024(T_W - 38) + 0.306 (T_W - 38)^{1.25}$$

As stated above, $Q_{IN} = \alpha(Q_{IT} + Q_{ILS} + Q_{IOS}) + Q_{DT} = 120.4 \text{ W}$, and $Q_{OUT} = Q_R + Q_{LT} + Q_{LS} + Q_{OS}$. Setting $Q_{IN} = Q_{OUT}$ and substituting produces:

$$120.4 \text{ W} = [1.34 \times 10^{-8} \{(T_W + 273)^4 - 9.35 \times 10^9\}] + [0.148 (T_W - 38)^{1.25}] + [0.041 (T_W - 38) + 0.315 (T_W - 38)^{1.25}] + [0.024 (T_W - 38) + 0.306 (T_W - 38)^{1.25}]$$

Which when reduced produces: