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REVISION 1

**CALCULATION OF RELEASES OF
RADIOACTIVE MATERIALS IN GASEOUS
LIQUID EFFLUENTS FROM BOILING WATER
REACTORS
(BWR-GALE CODE)**

~~E.P. Cardie, Editor~~
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**Office of Nuclear Reactor Regulation
U.S. Nuclear Regulatory Commission**

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**CALCULATION OF RELEASES OF RADIOACTIVE MATERIALS
IN GASEOUS AND LIQUID EFFLUENTS FROM
BOILING WATER REACTORS
(BWR-GALE CODE)**

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FOREWORD

The calculational procedures described in this NUREG report reflect current NRC staff practice. Therefore, the methods described herein will be used in the evaluation of applications for construction permits and operating licenses docketed after January 1, 1979, until this NUREG is revised as a result of additional staff review.

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CHAPTER 1. BWR-GALE CODE

1.1 INTRODUCTION

In promulgating Appendix I to 10 CFR Part 50, the U.S. Nuclear Regulatory Commission indicated its desire to use the best available data for improving the calculational models used by the Commission Staff to determine conformance with the requirements of the regulation. The first issue of this NUREG Report was published in April 1976. Revision 1 is being issued to update NUREG-0016 by incorporating more recent operating data now available and also by incorporating the results of a number of in-plant measurements programs at operating BWRs.

The BWR-GALE (Boiling Water Reactor Gaseous and Liquid Effluents) Code is a computerized mathematical model for calculating the release of radioactive material in gaseous and liquid effluents from boiling water reactors (BWRs). The calculations are based on data generated from operating reactors, field tests, laboratory tests, and plant-specific design considerations incorporated to reduce the quantity of radioactive materials that may be released to the environment.

The average quantity of radioactive material released to the environment from a nuclear power reactor during normal operation including anticipated operational occurrences is called the "source term," since it is the source or initial number used in calculating the environmental impact of radioactive releases. The calculations performed by the BWR-GALE Code are based on (1) standardized coolant activities derived from American Nuclear Society (ANS) 18.1 Working Group recommendations (Ref. 1), (2) release and transport mechanisms that result in the appearance of radioactive material in liquid and gaseous waste streams, (3) plant-specific design features used to reduce the quantities of radioactive materials ultimately released to the environs, and (4) information received on the operation of nuclear power plants.

In a BWR, water is converted to steam by heat from the fuel elements in the reactor. The steam expands through a turbine and then is condensed and returned to the reactor. The principal mechanisms that affect the concentrations of radioactive materials in the reactor coolant are (1) fission product leakage to the coolant from defects in the fuel cladding and fission product generation in tramp uranium, (2) corrosion products activated in the core, (3) radioactivity removed by the reactor coolant cleanup system, (4) radioactivity removed by the condensate demineralizers, (5) radioactivity removed through the steam-jet air ejectors, and (6) radioactivity removed due to reactor coolant leakage. These mechanisms are described briefly in the following paragraphs.

Fission products enter the coolant as a result of defects in the fuel cladding and from the tramp uranium on the cladding surfaces, while corrosion products are activated in the reactor core. These impurities must be continuously removed from the reactor coolant to prevent damage to the fuel elements and other reactor components. The removal is accomplished in two ways: (1) after passing through the turbine, the condensed steam is processed through the condensate cleanup system (e.g., demineralizers) and returned to the reactor for reuse and (2) a side stream of reactor coolant is continuously withdrawn, processed through the reactor water cleanup system (demineralizers), and returned to the reactor vessel. Both cleanup systems remove particulates and ionic impurities from the reactor coolant. The materials collected by the demineralizers are removed periodically by chemical regeneration or by replacement of resins. The liquid wastes are processed in the liquid waste treatment system, and the spent ion exchange resins are transferred to the solid waste treatment system and prepared for offsite shipment.

Radioactive gases are removed from the condensing steam in the main condenser by the steam-jet air ejectors. This source of gaseous waste is treated principally by delaying the release to permit radioactive decay. Treatment methods include holdup lines, long-term holdup using charcoal delay systems, and cryogenic distillation.

Additional radioactive material is released with the exhaust from the turbine gland sealing system when a sidestream of primary steam flows through the turbine gland seal. The steam is condensed and returned to the condenser hotwell for reuse in the reactor. However, noble gases, activation gases, radioactive particulates, and radioiodine that remain in the gaseous phase must be vented. The treatment provided this source of gaseous waste is normally a two-minute holdup line that permits decay of the short-lived noble and activation gases before they are released to the environment. Clean steam (nonradioactive steam) may be

used in place of primary steam to eliminate the turbine gland seal as a potential activity release point.

Following plant shutdowns, mechanical vacuum pumps are used to reestablish the main condenser vacuum. In addition, the mechanical vacuum pumps may be used during plant shutdowns to maintain a slight condenser vacuum and thereby prevent outleakage of radioactive gases from the main condenser. If required to meet the design objectives of Appendix I, the effluent from the mechanical vacuum pump effluent could be processed through charcoal adsorbers for removal of radioiodine prior to release to the environment.

In addition to the above release points, the BWR-GALE Code considers ventilation system releases from the turbine, containment, auxiliary (including the spent fuel pool area), and radwaste buildings due to leakage from contaminated systems. Such leakage from systems containing main steam or reactor coolant may have an appreciable effect on the radioactive source term. Leakage may occur through valve stems, pump seals, and flanged connections. The amount of airborne radioactive material released is a function of reactor coolant temperature, pressure, and activity at the point where the leak occurs. Included with the leaking steam or coolant are noble gases, iodine, and particulates that are released directly to the building atmosphere. In some cases, leakage may be reduced by special design features such as vacuum leakoff drains or "clean" steam on the valve bonnets in addition to normal precautions such as backseating valves and using all-welded systems. Leakage can also be reduced by the use of closed leakoff drains and by increased maintenance.

Liquid waste sources include liquid streams used to sluice (transfer), backwash, regenerate, and rinse demineralizer resins; laundry waste water; personnel shower wastes; laboratory drain wastes; decontamination wastes; and water collected in equipment drains and floor drains.

This chapter provides a step-by-step explanation of the BWR-GALE Code and a description of the parameters that have been built into the Code for use with all BWR source term calculations. These parameters, which apply generically to all BWRs, have been incorporated into the Code to eliminate the need for their entry on input data cards. This chapter also describes the entries required to be entered on input data cards used by the Code. Explanations of the data required, along with acceptable means for calculating such data, are given for each input data card. Chapter 2 gives the principal source term parameters developed for use with the BWR-GALE Code and explains the bases for each parameter. Chapter 3 contains a sample data input sheet and a FORTRAN listing of the BWR-GALE Code. Chapter 4 lists the information needed to generate source terms that an applicant is required to submit with the application.

1.2 DEFINITIONS

The following definitions apply to terms used in this report:

Activation Gases: The gases (including oxygen, nitrogen, and argon) that become radioactive due to irradiation in the core.

Anticipated Operational Occurrences - unplanned releases of radioactive materials from miscellaneous actions such as equipment failure, operator error, administrative error, that are not of consequence to be considered an accident.

Chemical Waste Stream: Liquids that contain relatively high concentrations of decontamination wastes or chemical compounds other than detergents. These liquids originate primarily from resin regenerants and laboratory waste.

Carryover Factor: Ratio of I-131 concentration in the condenser hotwell to its concentration in the reactor vessel. This value is used to express the partition coefficient between the steam and water phases in the reactor.

Decontamination Factor (DF): The ratio of the initial amount of a nuclide in a stream (specified in terms of concentration or activity of radioactive materials) to the final amount of that nuclide in a stream following treatment by a given process.

Detergent Waste Stream: Liquids that contain detergent, soaps, or similar organic materials. These liquids consist principally of laundry, personnel shower, and equipment decontamination wastes and normally have a low radioactivity content.

Effective Full Power Days: The number of days a plant would have to operate at 100% licensed power to produce the integrated thermal power output during a calendar year; i.e.,

$$\text{Effective Full Power Days} = \frac{\text{Integrated Thermal Power}}{\text{Licensed Power Level}} = \frac{\sum P_i T_i}{P_{\text{total}}}$$

where

P_i is the i th power level, in MWt;

P_{total} is the license power level, in MWt; and

T_i is the time of operation at power level i , in days.

Fission Product: A nuclide produced either by fission or by subsequent radioactive decay or neutron activation of the nuclides formed in the fission process.

Gaseous Effluent Stream: Gaseous waste containing radioactive materials resulting from the operation of a nuclear power reactor.

High-Purity Waste Stream: Liquids, normally of low conductivity, consisting primarily of liquid waste collected from building equipment drains, valve and pump seal leakoffs, demineralizer backwash, ultrasonic resin cleaning, and resin transfer. These liquids are normally reused as primary coolant makeup water after processing.

Liquid Effluent Stream: Liquid wastes containing radioactive materials resulting from the operation of a nuclear power reactor.

Low-Purity Waste Stream: Liquids, normally of high conductivity and not of primary coolant quality, collected from building sumps, uncollected valve and pump seal leakoffs, miscellaneous vents, and floor drains.

Partition Coefficient (PC): The ratio of the concentration of a nuclide in the gas phase to the concentration of that nuclide in the liquid phase when the liquid and gas are at equilibrium.

Plant Capacity Factor: The ratio of the average net power to the rated power capacity.

Radioactive Halogens: The radioactive isotopes of fluorine, chlorine, bromine, and iodine. The radioactive isotopes of iodine are the principal halogen isotopes considered in dose calculations.

Radioactive Noble Gases: The radioactive isotopes of helium, neon, argon, krypton, xenon, and radon, which are characterized by their chemical inactivity. The radioactive isotopes of krypton and xenon are the principal noble gas isotopes considered in dose calculations.

Reactor Coolant: The fluid circulated through the reactor to remove heat. In a BWR, the fluid is allowed to boil in the reactor vessel to generate steam and power the turbine. The reactor coolant activity is considered to be constant over a range of power levels, coolant and cleanup flows, and reactor coolant volumes. The radionuclide distributions and concentrations for the reactor coolant and main steam are based on the values given in American National Standard, ANSI N237, Source Term Specification, (Ref. 1) but have been adjusted to plants with pumped forward heater drains. In addition, radioiodine and noble gas concentrations are based on a recent compilation of available operating data. Therefore, the concentration values in NUREG-0016, Rev. 1 differ slightly from the ANSI N237 values. Provisions are made in the BWR-GALE Code, in accordance with the recommendations of the standard, for adjusting reactor coolant concentrations should the plant be designed to parameters that are outside the ranges considered in the standard. The ANSI N237 radionuclide concentrations used are also representative of measured values based on the available operating data. The radionuclides are divided into the following categories:

1. Noble gases
2. Halogens (Br, I)
3. Cesium and Rubidium
4. Water activation products
5. Tritium

6. Other nuclides (as listed in Table 2-2 of Chapter 2 of this document)

Regenerant Solutions Waste Stream: Liquids containing regeneration chemical compounds that originate from regeneration of the condensate demineralizer resins.

Source Term: The calculated annual average quantity of radioactive material released to the environment from a nuclear power reactor during normal operation including anticipated operational occurrences. The source term is the isotopic distribution of radioactive materials used in evaluating the impact of radioactive releases on the environment. Normal operation includes routine outages for maintenance and scheduled refuelings.

Tramp Uranium: The uranium present on the exterior of the cladding of a fuel rod and core support structure surfaces.

1.3 GASEOUS SOURCE TERMS

The following sources are considered in calculating the release of radioactive materials (noble gases, particulates, carbon-14, tritium, argon-41 and iodine) in gaseous effluents from normal operation including anticipated operational occurrences:

1. Main condenser offgas system,
2. Turbine gland sealing system,
3. Mechanical vacuum pumps, and
4. Ventilation exhaust air from the containment, auxiliary, radwaste, and turbine buildings, and the spent fuel pool area

The releases of radioactive materials in gaseous effluents are based on measurements made at operating BWRs. The radioactive particulate and noble gas release rates are specified in the BWR-GALE Code and are modified only as needed to reflect treatment processes. Gaseous releases for building ventilation exhaust systems and the main condenser offgas system are based on the average of actual measurements. Radioiodine releases are related to the iodine-131 reactor water concentrations for the BWR being evaluated.

Chapter 2 provides iodine and particulate decontamination factors for removal equipment and parameters for calculating holdup times for noble gases and for calculating tritium releases.

1.4 LIQUID SOURCE TERMS

The following sources are considered in calculating the release of radioactive materials in liquid effluents from normal operations including anticipated operational occurrences:

1. Processed liquid wastes from the high-purity waste system,
2. Processed liquid wastes from the low-purity waste system,
3. Processed liquid wastes from the chemical waste system,
4. Processed liquid regenerant wastes, and
5. Detergent wastes.

The radioactivity input to the liquid radwaste treatment system is based on flow rates of the liquid waste streams and their radioactivity levels, expressed as a fraction of the primary reactor coolant activity (PCA). The primary coolant activity (PCA) is based on the recommendations of American National Standard (ANSI N237) Source Term Specification, (Ref. 1), with the changes as noted in Section 1.2 under the Reactor Coolant definition.

Radionuclide removal by the liquid radwaste treatment system is based on the following parameters:

1. Decay during collection and processing and
2. Removal by the proposed treatment systems, e.g., filtration, ion exchange, evaporation, reverse osmosis, and plateout.

For BWRs using a deep-bed condensate demineralizer, the inventory of radionuclides collected on the demineralizer resins is calculated by considering the flow rate of condensate at main steam activity that is processed through the demineralizers and radionuclide removal using the decontamination factors given in Chapter 2. The radioactivity content of the demineralizer regenerant solution is obtained by considering that all of the activity that is collected by the condensate demineralizers is removed from the resins at the interval dictated by the regeneration frequency.

Methods for calculating collection and processing times and the decontamination factors for radwaste treatment equipment are given in this chapter. The liquid radioactive source terms are adjusted to compensate for equipment downtime and anticipated operational occurrences.

For plants having an onsite laundry, a standard detergent source term, adjusted for the treatment provided, is added to the adjusted source term.

1.5 INSTRUCTIONS FOR COMPLETING BWR-GALE CODE INPUT DATA CARDS

1.5.1 PARAMETERS INCLUDED IN THE BWR-GALE CODE

The parameters listed below are built into the BWR-GALE Code since they are generally applicable to all BWR source term calculations and do not require entry on input data cards.

1.5.1.1 Plant Capacity Factor

0.80 (292 effective full power days per year)

1.5.1.2 Radionuclide Concentrations in the Reactor Coolant and Main Steam

See Chapter 2, Tables 2-2 through 2-5 of this document.

1.5.1.3 Noble Gas, Radioiodine, and Particulate Releases From Building Ventilation Systems Prior to Treatment

See Tables 1-1 and 1-2. For a discussion of the normalization techniques see Section 2.2.4.

1.5.1.4 Radioiodine Input Rate to Main Condenser Offgas System

6 Ci/yr per reactor downstream of main condenser air ejectors.

1.5.1.5 Main Condenser Vacuum Pump Release

Xe-133 -- 1300 Ci/yr

Xe-135 -- 500 Ci/yr

I-131 -- See Table 1-3

1.5.1.6 Charcoal Delay Systems

For a charcoal delay system used to treat the offgases from the main condenser air ejector, the BWR-GALE Code calculates the holdup times for Kr and Xe. Iodine releases from charcoal delay systems are negligible due to the large quantities of charcoal used in the system. The holdup times for noble gases are calculated by the Code using the following equation and the data entered on Cards 29-32.

$$T = 43.1 \frac{MK}{P}$$

where

K is the dynamic adsorption coefficient, in cm^3/gm
(see chart on page 2-35);

M is the mass of charcoal, in 10^3 lbs

T is the holdup time, in hr, and

P is the thermal power level (MWt) entered in Card 2.

TABLE 1-1
GASEOUS RELEASES FROM VENTILATION SYSTEMS PRIOR TO TREATMENT
(in Ci/yr per Reactor)

<u>NUCLIDE</u>	<u>CONTAINMENT BUILDING</u>	<u>AUXILIARY BUILDING</u>	<u>TURBINE BUILDING</u>	<u>RADWASTE BUILDING</u>
Kr-83m	**	**	**	**
Kr-85m	1	3	25	**
Kr-85	**	**	**	**
Kr-87	**	2	61	**
Kr-88	1	3	91	**
Kr-89	**	2	580	29
Xe-131m	**	**	**	**
Xe-133m	**	**	**	**
Xe-133	27	83	150	220
Xe-135m	15	45	400	530
Xe-135	33	94	330	280
Xe-137	45	135	1000	83
Xe-138	2	6	1000	2
Cr-51*	0.0002	0.0009	0.0009	0.0007
Mn-54	0.0004	0.001	0.0006	0.004
Fe-59	0.00009	0.0003	0.0001	0.0003
Co-58	0.0001	0.0002	0.001	0.0002
Co-60	0.001	0.004	0.001	0.007
Zn-65	0.001	0.004	0.006	0.0003
Sr-89	0.00003	0.00002	0.006	NA
Sr-90	0.000003	0.000007	0.00002	NA
Zr-95	0.0003	0.0007	0.00004	0.0008
Nb-95	0.001	0.009	0.000006	0.000004
Mo-99	0.006	0.06	0.002	0.000003
Ru-103	0.0002	0.004	0.00005	0.000001
Ag-110m	0.0000004	0.000002	NA	NA
Sb-124	0.00002	0.00003	0.0001	0.00007
Cs-134	0.0007	0.004	0.0002	0.0024
Cs-136	0.0001	0.0004	0.0001	NA
Cs-137	0.001	0.005	0.001	0.004
Ba-140	0.002	0.02	0.010	0.000004
Ce-141	0.0002	0.0007	0.010	0.000007

*Particulate release rates are prior to filtration.

**Less than 1 Ci/yr per reactor.

NA Not Analyzed; analysis for the isotope was not performed.

TABLE 1-2

RADIOIODINE RELEASES FROM BUILDING VENTILATION
SYSTEMS PRIOR TO TREATMENT
(Ci/yr/ μ Ci/gm)

	<u>Containment Bldg**</u>	<u>Auxiliary Bldg**</u>	<u>Turbine Bldg***</u>	<u>Radwaste Bldg**</u>
Annual Normalized* Iodine Release Rate				
Power Operation	1.2	11.1	3.8×10^3	4.6
Refueling/Maintenance Outages	4.7	0.5	4.1×10^2	1.4

*The normalized release rate, expressed in grams of water during the modes of operation, represents the effective leak rate for radioiodine. It is the combination of the reactor water leakage rate into the building and the partitioning of the radioiodine between the water phase in the leakage and the gas phase where it is measured. For the turbine building the effective leak rate also includes the carryover for radioiodine from reactor water to steam in the reactor vessel.

**To obtain the actual iodine release from these bldgs in Ci/yr, multiply the normalized release by the coolant concentration in μ Ci/gm.

***To obtain the actual iodine release from the turbine building in Ci/yr, multiply the normalized release by the coolant concentration in μ Ci/gm and by the iodine carryover from Table 2-4.

TABLE 1-3

RADIOIODINE RELEASES FROM MECHANICAL VACUUM PUMP
(Ci/yr/ μ Ci/gm)

	<u>Annual Normalized* Iodine Release Rate**</u>
Short-term outages	4.9×10^2
Refueling/Maintenance Outages	1.1×10^3

*The normalized release rate, expressed in grams of water during the modes of operation, represents the effective leak rate for radioiodine. It is the combination of the reactor water leakage rate, the partitioning of the radioiodine between the water phase in the leakage and the gas phase where it is measured and the carryover for radioiodine from reactor water to steam in the reactor vessel.

**To obtain the actual iodine release from the mechanical vacuum pump in Ci/yr, multiply the normalized release by the coolant concentration in μ Ci/gm and by the iodine carryover from Table 2-4.

1.5.1.7 Cryogenic Distillation System

For a cryogenic distillation system, the BWR-GALE Code uses a partition coefficient of 0.0001 for Xe and I and 0.00025 for Kr to calculate Xe, I, and Kr removal during separation by distillation. The Xe, I, and Kr separated by distillation are considered to be released following 90-day holdup. The calculated releases are the sum of the noble gases and radioiodine released from the overheads during distillation without holdup and the noble gases and iodine released following 90-day holdup.

1.5.1.8 Decontamination Factors for Condensate Demineralizers

<u>Demineralizer</u>	<u>Anions</u>	<u>Cs, Rb</u>	<u>Other Nuclides</u>
Deep bed	10	2	10
Powdex	10	2	10

1.5.1.9 Detergent Wastes

The radionuclides listed in Table 2-28 of Chapter 2 are assumed to be released unless treatment is provided or laundry is not processed on site.

1.5.1.10 Tritium Releases

Total tritium release equals 0.03 Ci/yr per Mwt. The quantity of tritium released through the liquid pathway is 50% of the total quantity calculated to be available for release, and 50% is calculated to be released in gaseous effluents. Of that released in gaseous effluents, half is released from the turbine building ventilation system and half is released from the containment building ventilation system.

1.5.1.11 Argon-41 Releases

The argon-41 input to the main condenser offgas treatment system is 40 μ Ci/sec. The dynamic adsorption coefficients for argon-41 in charcoal delay beds are 6.4 cm^3/gm and 16 cm^3/gm for ambient and chilled temperature systems, respectively. The argon-41 release from purging or venting of the drywell is 15 Ci/yr.

1.5.1.12 Regeneration of Condensate Demineralizers

Flow rates and concentrations of radioactive materials routed to the liquid radwaste system from the chemical regeneration of the condensate demineralizers are based on the following parameters:

1. Liquid radioactivity flow to the demineralizer is based on the radioactivity of the main steam and the fraction of radioactivity which does not bypass the condensate demineralizers in the pumped forward flow.
2. All radionuclides removed from the condensate by the demineralizers are removed from the demineralizer resins during chemical regeneration. The regenerant waste radioactivity is adjusted for radionuclide decay during operation of the demineralizers.

1.5.1.13 Adjustment to Liquid Radwaste Source Terms for Anticipated Operational Occurrences

1. The calculated source term is increased by 0.1 Ci/yr per reactor using the same isotopic distribution as for the calculated source term to account for anticipated occurrences such as operator errors resulting in unplanned releases.

2. Evaporators are assumed to be unavailable for two consecutive days per week for maintenance. If a two-day holdup capacity or an alternative evaporator is available, no adjustment is needed. If less than a two-day capacity is available, the waste excess is assumed to be handled as follows:

- a. High-Purity or Low-Purity Waste--Processed through an alternative system (if available) using a discharge fraction consistent with the lower purity system.
- b. Chemical Waste--Discharged to the environment to the extent holdup capacity or an alternative evaporator is not available.

1.5.2 PARAMETERS REQUIRED FOR THE BWR-GALE CODE

The parameters described in the following sections must be entered on input data cards. Complete the cards designated below by "(SAR/ER)" from information given in the Safety Analysis and Environmental Reports. Complete the remaining cards (i.e., those not designated below as "(SAR/ER)" cards) using the principal source term parameters specified below and discussed in Chapter 2.

1.5.2.1 Card 1: Name of Reactor (SAR/ER)

Enter in spaces 33-60 the name of the reactor.

1.5.2.2 Card 2: Thermal Power Level (SAR/ER)

Enter in spaces 73-80 the maximum thermal power level (in MWt) evaluated for safety considerations in the Safety Analysis Report.

1.5.2.3 Card 3: Total Steam Flow Rate (SAR/ER)

Enter in spaces 73-80 the total steam flow rate from the reactor (in 10^6 lbs/hr).

1.5.2.4 Card 4: Mass of Coolant in Reactor Vessel (SAR/ER)

Enter in spaces 73-80 the mass of water in the reactor vessel and recirculation lines (in 10^6 lbs).

1.5.2.5 Card 5: Cleanup Demineralizer Flow (SAR/ER)

Enter in spaces 73-80 the reactor coolant flow rate (in 10^6 lbs/hr) through the reactor coolant cleanup system demineralizers.

1.5.2.6 Card 6: Condensate Demineralizer Regeneration Time

For deep-bed condensate demineralizers, use a 3.5-day regeneration frequency. If ultrasonic resin cleaning is used, assume 8-day regeneration frequency. Multiply the frequency by the total number of demineralizers and enter the calculated number of days in spaces 73-80. For filter/demineralizers (Powdex), enter 0.0 in spaces 73-80.

1.5.2.7 Card 7: Fraction of Feedwater Through Condensate Demineralizer (SAR/ER)

Enter in spaces 73-80 the fraction of feedwater processed through the condensate demineralizers.

1.5.2.8 Cards 8-19: Liquid Radwaste Treatment System Input Parameters

Four liquid radwaste inlet streams are considered in the BWR-GALE Code (see Section 1.5.2.22 for detergent wastes):

1. High-Purity Waste, Cards 8-10
2. Low-Purity Waste, Cards 11-13
3. Chemical Waste, Cards 14-16
4. Regenerant Solutions Waste, Cards 17-19

Three input data cards are used to define the major parameters for each of the four waste streams. Essentially the same information is needed on the three input data cards used for each of the four streams. The instructions given in this section are applicable to all four waste streams, with the following exception: the inlet waste activity is not entered on Card 17 for the regenerant solutions wastes for systems using regenerable condensate demineralizers since that activity is calculated by the Code.

The entries required on the first card (8, 11, and 14) for the High-Purity, Low-Purity, and Chemical Waste Systems, respectively, are outlined below and described in more detail in Section 1.5.2.8.1.

1. Enter in spaces 18-41 the name of the waste inlet stream (e.g., high-purity wastes).
2. Enter in spaces 42-49 the flow rate (in gal/day) of the inlet stream.
3. Enter in spaces 57-61 the activity of the inlet stream expressed as a fraction of the primary coolant activity (PCA).

On the first card for the Regenerant Solutions Waste System (i.e., Card 17), enter in spaces 73-80 the flow rate of the regenerant solutions waste inlet stream. For the calculation of liquid effluents for regeneration of demineralizers other than the condensate demineralizers, see Appendix A.

The second card (9, 12, 15, and 18) for each waste stream contains the overall system decontamination factors for three categories of radionuclides, as follows:

1. Enter in spaces 21-28 the DF for anions.
2. Enter in spaces 34-41 the DF for cesium and rubidium.
3. Enter in spaces 47-54 the DF for other nuclides.

The following entries are required on the third card (10, 13, 16, and 19) for each waste stream:

1. Enter in spaces 29-33 the waste collection time (in days) prior to processing.
2. Enter in spaces 48-53 the sum of the waste processing and discharge time (in days).
3. Enter in spaces 72-77 the average fraction of wastes to be discharged after processing.

The following sections explain in more detail the use of the parameters in this document and the information given in the SAR/ER to make the data entries in Cards 8-19 listed above.

1.5.2.8.1 Liquid Waste Flow Rates and Activities (Cards 8, 11, 14, and 17)

Calculate flow rates and activities to complete the first card for each liquid radwaste inlet stream by using the waste volumes and activities given in Table 1-4. To the input flow rates and activity given in the table, add expected flows and activities more specific to the plant design as given in the SAR/ER. The inlet streams should be combined to form the four principal waste streams (high-purity, low-purity, chemical wastes, and regenerant wastes) considered in this document. Calculate the primary coolant activity (PCA) of each of the four principal inlet streams (except for the regenerant waste as indicated above) by determining the weighted average activity of the composite stream entering the waste collection tanks. For example, if inlet streams A, B, and C enter the low-purity waste collector tank at average rates and PCA as listed below:

Stream A	1,000 gal/day at 0.01 PCA
Stream B	2,000 gal/day at 0.1 PCA
Stream C	500 gal/day at 1.0 PCA

the composite A, B, C activity would be calculated as follows:

$$\frac{(1000 \text{ gal/day})(0.01 \text{ PCA}) + (2000 \text{ gal/day})(0.1 \text{ PCA}) + (500 \text{ gal/day})(1.0 \text{ PCA})}{(1000 \text{ gal/day} + 2000 \text{ gal/day} + 500 \text{ gal/day})} = 0.2 \text{ PCA}$$

The entries on Card 11 for this example would then be: spaces 18-41, "Low-Purity Waste"; spaces 42-49, "3500"; spaces 57-61, "0.2."

TABLE 1-4
BWR LIQUID WASTES

SOURCE	EXPECTED DAILY AVERAGE INPUT FLOW RATE (in gal/day)		FRACTION OF THE PRIMARY COOLANT ACTIVITY (PCA)
	DEEP BED PLANT WITH ULTRASONIC RESIN CLEANER	DEEP BED PLANT WITHOUT ULTRASONIC RESIN CLEANER OR A FILTER/DEMINERALIZER PLANT	
<u>Equipment Drains</u>			
Drywell	3,400	3,400	1.00
Containment, auxiliary building, and fuel pool	3,700	3,700	0.1
Radwaste building	1,100	1,100	0.1
Turbine building	3,000	3,000	0.001
Ultrasonic resin cleaner	15,000	-	0.05
Resin rinse*	2,500	5,000	0.002
<u>Floor Drains</u>			
Drywell	700	700	0.001
Containment, auxiliary building, and fuel handling	2,000	2,000	0.001
Radwaste building	1,000	1,000	0.001
Turbine building	2,000	2,000	0.001
<u>Other Sources</u>			
Cleanup phase separator decant	640	640	0.002
Laundry drains	1,000	1,000	-
Lab drains	500	500	0.02
Regenerants*	1,700	3,400	**
Condensate demineralizer backwash†	-	8,100	2×10^{-6}
Chemical lab waste	100	100	0.02

* Deep-bed condensate demineralizers only.

** Calculated by BWR-GALE Code.

† Filter/demineralizer (Powdex) condensate demineralizers only.

The input flows and activities are entered in units of gal/day and fraction of PCA, respectively.

1.5.2.8.2 Decontamination Factors for Equipment Used in the Liquid Radwaste Treatment System (Cards 9, 12, 15, and 18)

The system decontamination factors (DFs) should be entered in the second card for each liquid radwaste inlet stream. The DFs represent the expected equipment performance averaged over the life of the plant. The following factors are to be considered in calculating overall decontamination factors for the various systems.

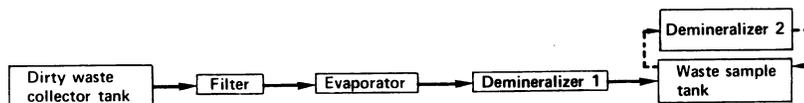
1. DFs are categorized by one of the following types of radionuclides:
 - a. Anions
 - b. Cs, Rb
 - c. Other nuclides

Note: A DF of 1 is assumed by the BWR-GALE Code for tritium. Dissolved noble gases and water activation products are not considered in the liquid code.

2. The system DF for each inlet stream is the product of the individual equipment DFs in each of the subsystems.
3. Equipment that is used optionally (as required) and not included in the normal flow scheme should not be considered in calculating the overall system DF.

Table 1-5 shows the decontamination factors to be used for BWR liquid waste treatment systems.

The following example illustrates the calculation of the decontamination factor for a low-purity waste treatment system: Assume that low-purity wastes are collected, processed through a filter, an evaporator, and a mixed-bed polishing demineralizer; and collected for sampling. If required to meet discharge criteria, the contents of the waste sample (test) tank are processed through a mixed-bed demineralizer for additional radionuclide removal. This example may be summarized schematically as:



Extracting from Table 1-5 gives the following values for the example:

	<u>Filter</u>	<u>Evaporator</u>	<u>Demineralizer 1</u>	<u>Demineralizer 2</u>	<u>Product</u>
Anions	1	10 ³	10	1	10 ⁴
Cs, Rb	1	10 ⁴	10	1	10 ⁵
Other Nuclides	1	10 ⁴	10	1	10 ⁵

These values were obtained as follows:

- ° A DF of 1.0 was applied to all nuclides for the filter.
- ° A DF of 10³ for anions and 10⁴ for Cs, Rb, and other nuclides was applied for the radwaste evaporator.
- ° A DF of 10 was applied for anions, Cs, Rb, and other nuclides for the evaporator condensate polishing demineralizer.
- ° A DF of 1 was applied to the second demineralizer since this demineralizer's use is optional and it is not used for normal operations.
- ° The product of the DFs was obtained by combining the first four columns for each radionuclide.

TABLE 1-5
DECONTAMINATION FACTORS FOR BWR LIQUID WASTE TREATMENT SYSTEMS

<u>TREATMENT SYSTEM</u>	<u>DECONTAMINATION FACTOR</u>		
<u>Demineralizers</u>	<u>Anion</u>	<u>Cs, Rb</u>	<u>Other Nuclides</u>
<u>Mixed-bed</u>			
Reactor Coolant Cleanup	10	2	10
Condensate (deep bed)	10	2	10
High-purity waste	$10^2(10)^*$	10(10)	$10^2(10)$
Low-Purity Waste	$10^2(10)$	2(10)	$10^2(10)$
Cation bed (any system)	1(1)	10(10)	$10^2(10)$
Anion bed (any system)	$10^2(10)$	1(1)	1(1)
Powdex (any system)	10(10)	2(10)	10(10)
<u>Evaporators</u>	<u>All Nuclides Except Anions</u>		<u>Anions</u>
Miscellaneous	10^4		10^3
Detergent wastes	10^2		10^2
<u>Reverse Osmosis</u>	<u>All Nuclides</u>		
Laundry wastes	30		
Other liquid wastes	10		
<u>Filters</u>	DF of 1.0 for all nuclides		

* For an evaporator polishing demineralizer or for the second demineralizer in series, the DF is given in parentheses.

Thus in Card 9 the following would be entered: in spaces 21-28, "10,000"; in spaces 34-41, "100,000"; and in spaces 47-54, "100,000."

1.5.2.8.3 Collection Time for Liquid Wastes (Cards 10, 13, 16, 19 -- Spaces 29-33)

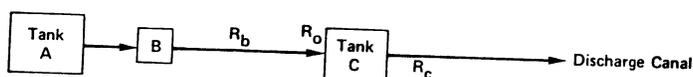
Collection time prior to processing is based on the input flow calculated above. Where redundant tanks are provided, assume the collection tank will be processed when filled to 80% capacity. If only one tank is provided, assume the tank will be processed when filled to 40% capacity. For example, if flow from a 1,000-gal/day floor drain is collected in two 20,000-gallon tanks prior to processing, collection time would be calculated as follows:

$$\text{Collection time } (T_c) = \frac{(20,000 \text{ gal})(0.8)}{1,000 \text{ gal/day}} = 16 \text{ days}$$

Then, for this example, "16" should be entered in spaces 29-33 on Card 13.

1.5.2.8.4 Processing and Discharge Time (Cards 10, 13, 16, 19 -- Spaces 48-53)

Decay during processing and discharge of liquid wastes is shown schematically as follows:



where

- A is the capacity of the initial tank in the flow scheme, in gal;
- B is the limiting process based on equipment flow capacity, dimensionless;
- C is the capacity of the final tank in the flow scheme prior to discharge, in gal;
- R_b is the equipment flow capacity of process B, in gal/day;
- R_c is the flow capacity of the Tank C discharge pump, in gal/day; and
- R_o is the rate of flow of additional wastes inputs to Tank C, in gal/day.

T_p , the process time credited for decay, is calculated as follows, in days:

$$T_p = \frac{0.8A}{R_b} \text{ for redundant tank, or } T_p = \frac{0.4A}{R_b} \text{ for a single tank}$$

T_d , the discharge time -- 50% credited for decay, is calculated as follows, in days:

$$T_d = \frac{0.8C}{R_c} \text{ for redundant tanks, or } T_d = \frac{0.4C}{R_c} \text{ for a single tank}$$

After performing the above two calculations, calculate whether credit may be taken for decay during processing and discharge by determining whether

$$0.8C > T_p(R_b + R_o) \text{ for redundant tanks, or } 0.4C > T_p(R_b + R_o) \text{ for a single tank}$$

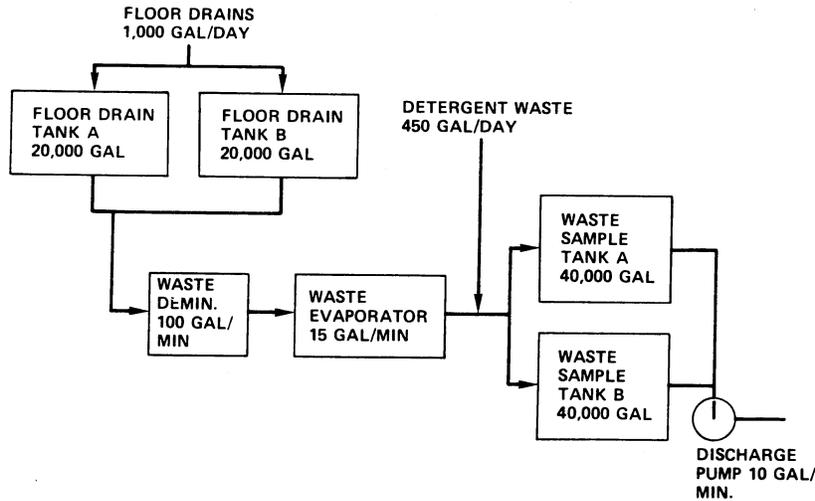
If so, then

$$\text{Decay} = (T_p + 0.5T_d)$$

where "Decay" is the new processing and discharge time to be entered in spaces 48-53 of the third card for each input stream (Cards 10, 13, 16, and 19).

If, however, $0.8C$ or $0.4C$ (as appropriate) $\leq T_p(R_b + R_o)$, T_p is used for the holdup time during processing, since Tank C may be discharged before Tank A has been completely processed. In this case, the T_p value should be entered in spaces 48-53 of the third card.

For example, for the following input waste stream:



Decay time during processing and discharge would be calculated as follows:

$$\text{Process Time } (T_p) = \frac{(0.8)(20,000 \text{ gal})}{(15 \text{ gal/min})(1440 \text{ min/day})} = 0.7 \text{ day}$$

$$\text{Discharge Time } (T_d) = \frac{(0.8)(40,000 \text{ gal})}{(10 \text{ gal/min})(1440 \text{ min/day})} = 2 \text{ days}$$

Then, checking for decay credit, $0.8C/(R_b + R_o) = 1.45$ days, which is greater than T_p ; therefore, credit is taken for $(T_p + 0.5T_d)$ or 1.7 days for processing and discharge. The input on spaces 48-53 to the Code is 1.7 days for processing and discharge time.

1.5.2.8.5 Fraction of Wastes Discharged (Cards 10, 13, 16, and 19 -- Spaces 72-77)

The percent of the wastes discharged after processing may vary between 1% and 100% based on the capability of the system to process liquid waste during equipment downtime, waste volume surges, tritium control requirements, and tank surge capacity. A minimum value of 1% discharge for high-purity wastes and 10% discharge for other wastes is used when the radwaste system is designed for maximum waste recycle, the system capacity is sufficient to process wastes for reuse during equipment downtime and anticipated operational occurrences, and a discharge route is provided.

The BWR-GALE Code calculates the release of radioactive materials in liquid waste from the four inlet streams after processing. Releases included in each stream are:

1. High-Purity Waste - Combined releases from equipment drains and sumps.
2. Low-Purity Waste - Combined releases from floor drains and sumps.
3. Chemical Waste - Combined releases from laboratory and decontamination wastes and from demineralizer regenerant solutions according to the design of the condensate demineralizer system. If a filter/demineralizer (Powdex) system is used, the laboratory and decontamination wastes are combined with the low-purity waste or solidified in the solid waste system.
4. Detergent Waste System - Combined releases from laundry operations, equipment decontamination solutions, and personnel decontamination showers.

1.5.2.9 Card 20: Gland Seal Steam Flow

Enter in spaces 73-80 of Card 20 the steam flow (in 10^3 lbs/hr) to the turbine gland seal, as follows:

1. If main steam is used for the sealing steam, enter a flow rate 0.001 times the main steam flow entered previously on Card 3.

2. If clean (nonradioactive) steam from an auxiliary boiler is used for sealing steam, enter 0.0 in spaces 73-80.

1.5.2.10 Card 21: Gland Seal Holdup Time (SAR/ER)

Enter in spaces 73-80 the design holdup time (in hr) for gases vented from the gland seal condenser.

1.5.2.11 Card 22: Holdup Time for Condenser Air Ejector Offgas (SAR/ER)

Enter in spaces 73-80 the design holdup time (in hr) for offgases from the main condenser air ejector prior to being processed through the offgas treatment system, e.g., a 10-minute holdup time prior to cryogenic distillation.

1.5.2.12 Card 23: Containment Building Releases

1. If ventilation exhaust air is treated through charcoal adsorbers which satisfy the guidelines of Regulatory Guide 1.140 (Ref. 2), enter the appropriate removal efficiency in spaces 43-46 for radioiodine corresponding to the depth of charcoal as indicated in Table 1-6.

2. If ventilation exhaust air is treated through HEPA filters which satisfy the guidelines of Regulatory Guide 1.140 (Ref. 2), enter a removal efficiency of 99. for particulates in spaces 53-56.

3. If no treatment is provided for the ventilation exhaust air to remove radioiodine or if the charcoal adsorbers do not satisfy the guidelines of Regulatory Guide 1.140 (Ref. 2), enter 0.0 in spaces 43-46; if no treatment is provided to remove particulates or if the HEPA filters do not satisfy the guidelines of Regulatory Guide 1.140 (Ref. 2), enter 0.0 in spaces 53-56.

1.5.2.13 Card 24: Turbine Building Releases

1. If ventilation exhaust air is treated through charcoal adsorbers which satisfy the guidelines of Regulatory Guide 1.140 (Ref. 2), enter the appropriate removal efficiency in spaces 43-46 for radioiodine corresponding to the depth of charcoal as indicated in Table 1-6.

2. If ventilation exhaust air is treated through HEPA filters which satisfy the guidelines of Regulatory Guide 1.140 (Ref. 2), enter a removal efficiency of 99. for particulates in spaces 53-56.

3. If no treatment is provided for the ventilation exhaust air to remove radioiodine or if the charcoal adsorbers do not satisfy the guidelines of Regulatory Guide 1.140 (Ref. 2), enter 0.0 in spaces 43-46; if no treatment is provided to remove particulates or if the HEPA filters do not satisfy the guidelines of Regulatory Guide 1.140 (Ref. 2), enter 0.0 in spaces 53-56.

1.5.2.14 Card 25: Fraction of Radioiodine Released from Turbine Gland Seal Condenser Vent

1. If, prior to release, the offgases from the turbine gland seal condenser vent are processed through charcoal adsorbers which satisfy the guidelines of Regulatory Guide 1.140 (Ref. 2), enter the removal efficiency in spaces 73-80 for radioiodine corresponding to the depth of charcoal as indicated in Table 1-6.

2. If the offgases are released from the turbine gland seal condenser without treatment, if clean steam is used, or if charcoal adsorbers provided do not satisfy the guidelines of Regulatory Guide 1.140 (Ref. 2), enter 0.0 in spaces 73-80.

TABLE 1-6

ASSIGNED REMOVAL EFFICIENCIES FOR CHARCOAL ADSORBERS
FOR RADIOIODINE REMOVAL

<u>Activated Carbon^a Bed Depth</u>	<u>Removal Efficiencies^b for Radioiodine %</u>
2 inches. Air filtration system designed to operate inside reactor containment	90.
2 inches. Air filtration system designed to operate outside the reactor containment and relative humidity is controlled at 70%.	70.
4 inches. Air filtration system designed to operate outside the reactor containment and relative humidity is controlled at 70%	90.
6 inches. Air filtration system designed to operate outside the reactor containment and relative humidity is controlled to 70%.	99.

^aMultiple beds, e.g., two 2-inch beds in series, should be treated as a single bed of aggregate depth of 4 inches.

^bThe removal efficiencies assigned HEPA filters for particulate removal and charcoal adsorbers for radioiodine removal are based on the design, testing and maintenance criteria recommended in Regulatory Guide 1.140, "Design, Testing and Maintenance Criteria for Normal Ventilation Exhaust System Air Filtration and Adsorption Units of Light-Water-Cooled Nuclear Power Plants" (Ref. 2).

1.5.2.15 Card 26 Fraction of Radioiodine Released from the Condenser Air Ejector Offgas Treatment System

1. If, prior to release, the offgases are processed through charcoal adsorbers which satisfy the guidelines of Regulatory Guide 1.140 (Ref. 2), enter the removal efficiency in spaces 73-80 for radioiodine corresponding to the depth of charcoal as indicated in Table 1-6.
2. If the offgas is released without treatment or through charcoal adsorbers that do not satisfy the guidelines of Regulatory Guide 1.140 (Ref. 2), enter 0.0 in spaces 73-80.
3. Enter a 1. in spaces 73-80 if the offgas is processed through a charcoal delay system.
4. If the offgas is processed through a cryogenic distillation system (removal of iodine by the cryogenic distillation system is built into the Code -see Card 29), enter 0.0 in spaces 73-80.

1.5.2.16 Card 27: Auxiliary Building Releases

1. If ventilation exhaust air is treated through charcoal adsorbers which satisfy the guidelines of Regulatory Guide 1.140 (Ref. 2), enter the appropriate removal efficiency in spaces 43-46 for radioiodine corresponding to the depth of charcoal as indicated in Table 1-6.
2. If ventilation exhaust air is treated through HEPA filters which satisfy the guidelines of Regulatory Guide 1.140 (Ref. 2), enter a removal efficiency of 99. for particulates in spaces 53-56.
3. If no treatment is provided for the ventilation exhaust air to remove radioiodine or if the charcoal adsorbers do not satisfy the guidelines of Regulatory Guide 1.140 (Ref. 2), enter 0.0 in spaces 43-46; if no treatment is provided to remove particulates or if the HEPA filters do not satisfy the guidelines of Regulatory Guide 1.140 (Ref. 2), enter 0.0 in spaces 53-56.

1.5.2.17 Card 28: Radwaste Building Releases

1. If ventilation exhaust air is treated through charcoal adsorbers which satisfy the guidelines of Regulatory Guide 1.140 (Ref. 2), enter the appropriate removal efficiency in spaces 43-46 for radioiodine corresponding to the depth of charcoal as indicated in Table 1-6.
2. If ventilation exhaust air is treated through HEPA filters which satisfy the guidelines of Regulatory Guide 1.140 (Ref. 2), enter a removal efficiency of 99. for particulates in spaces 53-56.
3. If no treatment is provided for the ventilation exhaust air to remove radioiodine or if the charcoal adsorbers do not satisfy the guidelines of Regulatory Guide 1.140 (Ref. 2), enter 0.0 in spaces 43-46; if no treatment is provided to remove particulates or if the HEPA filters do not satisfy the guidelines of Regulatory Guide 1.140 (Ref. 2), enter 0.0 in spaces 53-56.

1.5.2.18 Card 29: Condenser Air Ejector Offgas Treatment System (SAR/ER)

1. Enter 1 in space 80 if a charcoal delay system is used to treat the offgas from the condenser air ejector.
2. Enter 2 in space 80 if the offgas from the condenser air ejector is processed by a cryogenic distillation system.
3. Enter a zero in space 80 if the offgas is not treated either through a charcoal delay system or by cryogenic distillation.

Note: Enter 0.0 on Cards 30, 31, and 32 if a charcoal delay system is not used to treat the offgases from the condenser air ejector.

1.5.2.19 Card 30: Dynamic Adsorption Coefficient for Krypton

Enter in spaces 73-80 the dynamic adsorption coefficient for Kr based on the system design and the dynamic adsorption coefficients noted below.

<u>DYNAMIC ADSORPTION COEFFICIENT (cm³/gm)</u>				
	<u>OPERATING 77°F</u> <u>DEW POINT 45°F</u>	<u>OPERATING 77°F</u> <u>DEW POINT 0°F</u>	<u>OPERATING 77°F</u> <u>DEW POINT -40°F</u>	<u>OPERATING 0°F</u> <u>DEW POINT -20°F</u>
Kr	18.5	25.	70.	105.

1.5.2.20 Card 31: Dynamic Adsorption Coefficient for Xenon

Enter in spaces 73-80 the dynamic adsorption coefficient for Xe based on the system design and dynamic adsorption coefficients noted below.

<u>DYNAMIC ADSORPTION COEFFICIENT (cm³/gm)</u>				
	<u>OPERATING 77°F</u> <u>DEW POINT 45°F</u>	<u>OPERATING 77°F</u> <u>DEW POINT 0°F</u>	<u>OPERATING 77°F</u> <u>DEW POINT - 40°F</u>	<u>OPERATING 0°F</u> <u>DEW POINT -20°F</u>
Xe	330.	440.	1160.	2410.

1.5.2.21 Card 32: Mass of Charcoal in Charcoal Delay System (SAR/ER)

Enter in spaces 73-80 the mass of charcoal (in 10³ lbs) used in the charcoal delay system.

1.5.2.22 Card 33: Detergent Waste

1. If the plant does not have an onsite laundry, enter 0.0 in spaces 73-80.
2. If the plant has an onsite laundry and detergent wastes are released without treatment, enter 1.0 in spaces 73-80.
3. If detergent wastes are treated prior to discharge, enter the decontamination factor in spaces 73-80. The parameters in Chapter 2 are used in determining the DF for the treatment applied to detergent waste.

CHAPTER 2. PRINCIPAL PARAMETERS USED
IN BWR SOURCE TERM CALCULATIONS AND THEIR BASES

2.1 INTRODUCTION

The principal parameters used in source term calculations have been compiled to standardize the calculation of radioactive source terms.

The following sections describe parameters used in the evaluation of radwaste treatment systems. The parameters have been derived from reactor operating experience where data were available. Where operating data were inconclusive or not available, information was drawn from laboratory and field tests and from engineering judgment. The bases for the source term parameters explain the reasons for choosing the numerical values listed. A list of references used in developing the parameters is also included.

The parameters in the BWR-GALE Code are updated periodically and published in revisions to this NUREG as additional operating data become available. The source term parameters used are believed to provide a realistic assessment of reactor and radwaste system operation.

2.2 PRINCIPAL PARAMETERS AND THEIR BASES

2.2.1 THERMAL POWER LEVEL

2.2.1.1 Parameter

The maximum thermal power level (MWt) evaluated for safety considerations in the Safety Analysis Report.

2.2.1.2 Bases

The power level used in the source term BWR-GALE Code is the maximum power level evaluated for safety considerations in the Safety Analysis Report. Using this value, the evaluation of the radwaste management systems need not be repeated when the applicant applies for a stretch power license at a later date. Past experience indicates that most utilities request approval to operate at maximum power soon after reaching commercial operation.

2.2.2 PLANT CAPACITY FACTOR

2.2.2.1 Parameter

A plant capacity factor of 80% is used, i.e., 292 effective full power days.

2.2.2.2 Bases

The source term calculations are based on a plant capacity factor of 80% averaged over the 30-year operating life of the plant, i.e., the plant operates at 100% power 80% of the time. The plant capacity factors experienced at BWRs are listed in Table 2-1 for the period 1972 through 1977.

The average plant capacity factors shown in Table 2-1 indicate that the 80% factor assumed is higher than the average factors experienced. However, it is expected that the major maintenance problems and extended refueling outages that have contributed to the lower plant capacity factors will be overcome and that the plants will achieve the 80% capacity factor when averaged over 30 years of operation.

2.2.3 RADIONUCLIDE CONCENTRATIONS IN THE REACTOR COOLANT

2.2.3.1 Parameter

As used in the BWR-GALE Code, Table 2-2 lists the expected radionuclide concentrations in the reactor coolant and steam for BWRs with design parameters within the ranges listed in Table 2-3. Should any design parameter be outside the ranges in Table 2-3, the BWR-GALE Code adjusts the concentrations in Table 2-2, using the factors in Tables 2-4 and 2-5. Figure 2-1 shows the graphical relationship of the design parameters.

TABLE 2-1
PLANT CAPACITY FACTORS AT OPERATING BWRs^a

<u>FACILITY^b</u>	<u>DATE OF COMMERICAL OPERATION^c</u>	<u>1972</u>	<u>1973</u>	<u>1974</u>	<u>1975</u>	<u>1976</u>	<u>1977</u>
Oyster Creek	12/69	77	65	66	58	70	58 ^e
Nine Mile Point-1	12/69	62	68	63	60	81	57 ^f
Millstone-1	03/71	55	34 ^d	63	68	66	84
Monticello	06/71	74	68	57	61	84	75
Dresden-3	11/71	67	54	47 ^e	33 ^f	60	76
Dresden-2	06/72		74	51	44 ^f	66	54
Vermont Yankee	11/72		44 ^e	59	81	73	80
Pilgrim-1	12/72		72	34 ^f	46 ^e	43 ^f	47 ^f
Quad Cities-1	02/73			51 ^f	65	52 ^f	55 ^e
Quad Cities-2	03/73			68	40 ^f	66	67
Cooper	07/74				60	57	70
Peach Bottom-2	07/74				57	61	45 ^f
Peach Bottom-3	12/74				59	67	54 ^f
Duane Arnold	02/75					55	67
Fitzpatrick	07/75					59	55 ^f
Brunswick-2	11/75					37 ^g	35 ^g
Hatch-1	12/75					65	57
	AVERAGE	67	67	61	63	66	70

^aFrom Semi-Annual Operating Reports for each facility, as submitted by respective licensees.

^bBig Rock Point, Dresden 1, Humboldt Bay, and Lacrosse are not included since they are small reactors (< 700 Mwt) and are not considered to be typical of modern-day reactors. Browns Ferry 1, 2 are not included since they were not operating due to fire.

^cPlant capacity factors listed begin with the first full year of commercial operation.

^dNot included due to extended maintenance outage to replace feedwater sparger.

^eNot included due to extended operation at reduced power.

^fNot included due to extended refueling outage.

^gNot included due to extended maintenance outage to correct power monitor tube vibrations.

TABLE 2-2
 RADIONUCLIDE CONCENTRATIONS
 IN BOILING WATER REACTOR COOLANT AND MAIN STEAM*
 (in $\mu\text{Ci/gm}$)

<u>ISOTOPE</u>	<u>REACTOR COOLANT</u>	<u>REACTOR STEAM</u>
<u>Noble Gases</u>		
Kr-83m		9.1(-4)**
Kr-85m		1.6(-3)
Kr-85		5.0(-6)
Kr-87		5.5(-3)
Kr-88		5.5(-3)
Kr-89		3.4(-2)
Kr-90		7.5(-2)
Kr-91		9.1(-2)
Kr-92		9.1(-2)
Kr-93		2.4(-2)
Kr-94		5.9(-3)
Kr-95		5.5(-4)
Kr-97		3.6(-6)
Xe-131m		3.9(-6)
Xe-133m		7.5(-5)
Xe-133		2.1(-3)
Xe-135m		7.0(-3)
Xe-135		6.0(-3)
Xe-137		3.9(-2)
Xe-138		2.3(-2)
Xe-139		7.5(-2)
Xe-140		8.0(-2)
Xe-141		6.5(-2)
Xe-142		1.9(-2)
Xe-143		3.2(-3)
Xe-144		1.5(-4)
<u>Halogens</u>		
Br-83	6(-3)	9(-5)***
Br-84	7(-3)	1(-4)
Br-85	3(-3)	5(-5)
I-131	3.7(-3)	6(-5)
I-132	6(-2)	9(-4)
I-133	5(-2)	8(-4)
I-134	1(-1)	2(-3)
I-135	5(-2)	8(-4)
<u>Cesium and Rubidium</u>		
Rb-89	5(-3)	5(-6)
Cs-134	3(-5)	3(-8)
Cs-136	2(-5)	2(-8)
Cs-137	8(-5)	8(-8)
Cs-138	1(-2)	1(-5)

*The reactor coolant concentration is specified at the nozzle where reactor water leaves the reactor vessel. Similarly, the reactor steam concentration is specified at time 0 at the nozzle.

** $1.1(-3) = 1.1 \times 10^{-3}$.

***Halogen concentrations listed in reactor steam are based on a carryover of 0.015. For a carryover of 0.004 the halogen reactor steam concentrations would be reduced proportionately.

TABLE 2-2 (Continued)

<u>ISOTOPE</u>	<u>REACTOR COOLANT</u>	<u>REACTOR STEAM</u>
<u>Water Activation Products</u>		
N-13	5(-2)	7(-3)
N-16	6(+1)	5(+1)
N-17	9(-3)	2(-2)
O-19	7(-1)	2(-1)
F-18	4(-3)	4(-3)
<u>Tritium*</u>		
H-3	1(-2)	1(-2)
<u>Other Nuclides</u>		
Na-24	1(-2)	1(-5)
P-32	2(-4)	2(-7)
Cr-51	6(-3)	6(-6)
Mn-54	7(-5)	7(-8)
Mn-56	5(-2)	5(-5)
Fe-55	1(-3)	1(-6)
Fe-59	3(-5)	3(-8)
Co-58	2(-4)	2(-7)
Co-60	4(-4)	4(-7)
Ni-63	1(-6)	1(-9)
Ni-65	3(-4)	3(-7)
Cu-64	3(-2)	3(-5)
Zn-65	2(-4)	2(-7)
Zn-69	2(-3)	2(-6)
Sr-89	1(-4)	1(-7)
Sr-90	7(-6)	7(-9)
Sr-91	4(-3)	4(-6)
Sr-92	1(-2)	1(-5)
Y-91	4(-5)	4(-8)
Y-92	6(-3)	6(-6)
Y-93	4(-3)	4(-6)
Zr-95	8(-6)	8(-9)
Zr-97	6(-6)	6(-9)
Nb-95	8(-6)	8(-9)
Nb-98	4(-3)	4(-6)
Mo-99	2(-3)	2(-6)
Tc-99m	2(-2)	2(-5)
Tc-101	9(-2)	9(-5)
Tc-104	8(-2)	8(-5)
Ru-103	2(-5)	2(-8)
Ru-105	2(-3)	2(-6)
Ru-106	3(-6)	3(-9)
Ag-110m	1(-6)	1(-9)
Te-129m	4(-5)	4(-8)
Te-131m	1(-4)	1(-7)

* Measured values increased to account for liquid recycle.

TABLE 2-2 (Continued)

<u>ISOTOPES</u>	<u>REACTOR COOLANT</u>	<u>REACTOR STEAM</u>
Te-132	1(-5)	1(-8)
Ba139	1(-2)	1(-5)
Ba140	4(-4)	4(-7)
Ba-141	1(-2)	1(-5)
Ba-142	6(-3)	6(-6)
La-142	5(-3)	5(-6)
Ce-141	3(-5)	3(-8)
Ce-143	3(-5)	3(-8)
Ce-144	3(-6)	3(-9)
Pr-143	4(-5)	4(-8)
Nd-147	3(-6)	3(-9)
W-187	3(-4)	3(-7)
Np-239	8(-3)	8(-6)

TABLE 2-3
PARAMETERS USED TO DESCRIBE THE REFERENCE BOILING WATER REACTOR

<u>PARAMETER</u>	<u>SYMBOL</u>	<u>UNITS</u>	<u>NOMINAL VALUE</u>	<u>RANGE</u>	
				<u>MAXIMUM</u>	<u>MINIMUM</u>
Thermal power	P	Mwt	3400	3800	3000
Weight of water in the reactor vessel	WP	lb	3.8(5)*	4.2(5)	3.4(5)
Cleanup demineralizer flow rate	FA	lb/hr	1.3(5)	1.5(5)	1.1(5)
Steam flow rate	FS	lb/hr	1.5(7)	1.7(7)	1.3(7)
Ratio of condensate demineralizer flow rate to steam flow rate	NC**	-	0.75	0.99	0.5

* $3.8(5) = 3.8 \times 10^5$

** For a BWR that is within the range indicated above, i.e. a BWR with pumped forward feedwater heater drains, the value for NC used in the BWR-GALE Code is 0.18 for iodine and 0.01 for Cs, Rb and other nuclides, as discussed on page 2-11. For a BWR that has a ratio of condensate demineralizer flow rate to steam flow rate equal to 1.0, i.e., full flow condensate demineralizers, a value of NC=1.0 is used in the BWR-GALE Code.

TABLE 2-4
VALUES USED IN DETERMINING ADJUSTMENT FACTORS FOR
BOILING WATER REACTORS

<u>SYMBOL</u>	<u>DESCRIPTION</u>	<u>NOBLE GASES</u>	<u>HALOGENS</u>	<u>Cs, Rb</u>	<u>WATER ACTIVATION PRODUCTS</u>	<u>TRITIUM</u>	<u>OTHER NUCLIDES</u>
NA	Fraction of material removed in the reactor water cleanup system	0.0	0.9	0.5	0.0	0.0	0.9*
NB	Fraction of material removed by the condensate demineralizers	0.0	0.9	0.5	0.0	0.0	0.9*
NS	Ratio of concentration in reactor steam to the concentration in reactor water	**	0.015 ^{†††}	0.001	***	1.0	0.001
R	Removal rate from the reactor water (hr ⁻¹).	**	0.40	0.17	***	††	0.31

* These represent effective removal terms and include other mechanisms such as plateout. Plateout would be applicable to nuclides such as Mo and corrosion products.

** All noble gases released from the core are transported rapidly out of the reactor water to the reactor steam and are stripped from the system in the main condenser. Therefore the concentration in the reactor water is negligible and the steam concentration is approximately equivalent to the ratio of the release rate and the steam flow rate.

*** Water activation products exhibit varying chemical and physical properties in reactor coolant which are not well defined. However, most are stripped off as gases. They are not effectively removed by the demineralizers of the systems, but their concentrations are controlled by decay.

+ These values of R apply to the reference BWR whose parameters are given in Table 2-3 and have been used in developing Table 2-5. For BWRs not included in Table 2-3, the appropriate value for R is determined by the BWR-GALE Code using the following equation:

$$R = \frac{FA \cdot NA + NC \cdot FS \cdot NS \cdot NB}{WP} \text{ for halogens, Cs, Rb, and other nuclides}$$

where the symbols are defined in this table, Table 2-3 and Figure 2-1. The values for R for noble gases and water activation products are not used in the adjustment factors of Table 2-5.

†† The tritium concentrations in the reactor water and the steam are expected to be equal. They are controlled by loss of water from the main coolant system by evaporation or leakage.

††† The value of 0.015 is used for BWRs which have Deep Bed Condensate Treatment. A value of 0.015 is also used for BWRs with Powdex Condensate Treatment and stainless steel condenser tubing. For BWRs which have Powdex Condensate Treatment systems and copper condenser tubing, a value of 0.004 should be used.

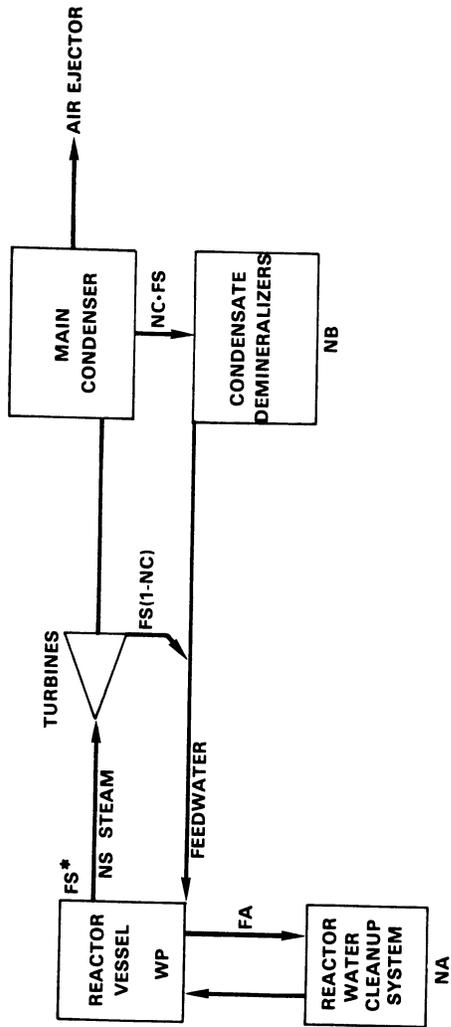
TABLE 2-5
ADJUSTMENT FACTORS FOR BOILING WATER REACTORS

<u>NUCLIDES</u>	<u>REACTOR COOLANT</u>	<u>REACTOR STEAM</u>
Noble gases*	1.0	1.0
Halogens**	$\frac{P}{WP} \left(110 \frac{1b}{MWT} \right) \frac{0.40 + \lambda}{R + \lambda}$	$\frac{P}{WP} \left(110 \frac{1b}{MWT} \right) \frac{0.40 + \lambda}{R + \lambda}$
Cs, Rb	$\frac{P}{WP} \left(110 \frac{1b}{MWT} \right) \frac{0.17 + \lambda}{R + \lambda}$	$\frac{P}{WP} \left(110 \frac{1b}{MWT} \right) \frac{0.17 + \lambda}{R + \lambda}$
Water activation products	1.0	1.0
Tritium***	1.0	1.0
Other nuclides	$\frac{P}{WP} \left(110 \frac{1b}{MWT} \right) \frac{0.31 + \lambda}{R + \lambda}$	$\frac{P}{WP} \left(110 \frac{1b}{MWT} \right) \frac{0.31 + \lambda}{R + \lambda}$

*Assumes that the ratio of power to steam flow is essentially the same for all BWRs.

** λ is the isotope's decay constant (hr^{-1}).

***The tritium concentrations in the reactor coolant and the steam are expected to be equal. They are controlled by loss of water from the main coolant system by evaporation or leakage. The concentration is therefore given by the ratio of the appearance rate in the coolant, which is about 100 Ci/yr, and the total loss from the system.



* SYMBOLS ARE DEFINED IN TABLES 2-3 AND 2-4

FIGURE 2-1
REMOVAL PATHS FOR THE REFERENCE
BOILING WATER REACTOR

2.2.3.2 Bases

The radionuclide concentrations, adjustment factors, and procedures for effecting adjustments are based on the values and methods in American National Standard ANSI N237, Source Term Specification, (Ref. 1) with the changes noted in Section 1.2 under the Reactor Coolant definitions. The values in Table 2-2 provide a set of typical radionuclide concentrations in the reactor coolant and steam for reactor designs within the parameters specified in Table 2-3. The values in Table 2-2 were those determined to be representative of radionuclide concentrations in a BWR over its lifetime based on the currently available data and models (Refs. 3 and 4). It is recognized that some systems will have design parameters that are outside the ranges specified in Table 2-3. For that reason a means of adjusting the concentrations to the actual design parameters has been provided in the BWR-GALE Code based on factors presented in Tables 2-4 and 2-5. The adjustment factors in Tables 2-4 and 2-5 are based on the following expression:

$$C = \frac{s}{w(\lambda + R)k}$$

where

- C is the specific activity, in $\mu\text{Ci/gm}$;
- k is a conversion factor, 454 gm/lbs;
- R is the removal rate of the isotope from the system due to demineralization, leakage, etc., in hr^{-1} ;
- s is the rate of release to and/or production of the isotope in the system, in $\mu\text{Ci/hr}$;
- w is the fluid weight, in lb; and
- λ is the decay constant, in hr^{-1} .

The following sample calculations illustrate the method by which the BWR-GALE Code will adjust the radionuclide concentrations in Table 2-2. As indicated in Table 2-5, adjustment factors will be calculated only for halogens, Cs, Rb, and other nuclides.

As an example, the sample case parameters shown below compare with the range of values in Table 2-3 as follows:

<u>Parameter</u>	<u>Sample Case Value</u>	<u>Range Values</u>
Thermal power level (Mwt)	3758	3000-3800
Water weight in vessel (lbs)	4.9×10^5	$3.4 \times 10^5 - 4.2 \times 10^5$
Cleanup demineralizer flow (lbs/hr)	1.5×10^5	$1.1 \times 10^5 - 1.5 \times 10^5$
Steam flow rate (lbs/hr)	15.4×10^6	$13.0 \times 10^6 - 17.0 \times 10^6$
Condensate demineralizer flow fraction	0.75	0.5 - 0.99

Since in this example one of the parameters (water weight in vessel) is outside the range, adjusted values of the three types of radionuclide concentrations are calculated using the actual value of each parameter, as follows:

1. Halogens (I-131 is used as an example) -- Using the equation for halogens in Table 2-5, the adjustment factor A is calculated as follows:

$$A = \frac{P}{WP} (110) \frac{0.40 + \lambda}{R + \lambda} \quad (2-1)$$

where the terms in the equation are as defined in Tables 2-3 and 2-4.

In calculating A, the variable R is calculated first, using the equation given in Table 2-4:

$$R = \frac{FA NA + NC FS NS NB}{WP} \quad (2-2)$$

where the terms in the equation are as defined in Tables 2-3 and 2-4.

Using the sample case parameters given above, the halogen parameters given in Table 2-4, and the pumped forward parameter given in Table 2-3, and substituting in Equation (2-2) gives

$$R = \frac{1.5 \times 10^5 \times 0.9 + 0.18 \times 15.4 \times 10^6 \times 0.015 \times 0.9}{4.9 \times 10^5} = 0.35$$

Then, using this value of R in Equation (2-1):

$$A = \frac{3758}{4.9 \times 10^5} (110) \frac{0.40 + 3.6 \times 10^{-3}}{0.35 + 3.6 \times 10^{-3}} = 0.96$$

The adjusted I-131 concentration

$$\begin{aligned} &= (\text{adjustment factor}) \times (\text{standard I-131 concentration}) \\ &= 0.96 \times 4 \times 10^{-3} \text{ } \mu\text{Ci/g} = 3.8 \times 10^{-3} \text{ } \mu\text{Ci/gm} \end{aligned}$$

2. Cs, Rb (Cs-137 is used as an example) -- Using the equation for Cs and Rb in Table 2-5, the adjustment factor A is calculated as follows:

$$A = \frac{P}{WP} (110) \frac{0.17 + \lambda}{R + \lambda} \quad (2-3)$$

where the terms in the equation are as defined in Tables 2-3 and 2-4.

In calculating A, the variable R is calculated first, using Equation (2-2). The Cs and Rb parameters given in Table 2-4, the pumped forward parameter given in Table 2-3, and the sample case parameters are used in the equation.

$$R = \frac{1.5 \times 10^5 \times 0.5 + 0.01 \times 15.4 \times 10^6 \times 0.001 \times 0.5}{4.9 \times 10^5} = 0.15$$

Then, using this value of R in Equation (2-3) above:

$$A = \left(\frac{3758}{4.9 \times 10^5} \right) (110) \left(\frac{0.17 + 2.6 \times 10^{-6}}{0.15 + 2.6 \times 10^{-6}} \right) = 0.96$$

The adjusted Cs-137 concentration

$$\begin{aligned} &= (\text{adjustment factor}) \times (\text{standard Cs-137 concentration}) \\ &= 0.96 \times 8 \times 10^{-5} \text{ } \mu\text{Ci/g} = 7.6 \times 10^{-5} \text{ } \mu\text{Ci/gm} \end{aligned}$$

3. Other Nuclides (Na-24 is used as an example) -- Using the equation for other nuclides in Table 2-5, the adjustment factor A is calculated as follows:

$$A = \frac{P}{WP} (110) \frac{0.31 + \lambda}{R + \lambda} \quad (2-4)$$

where the terms in the equation are as defined in Tables 2-3 and 2-4.

In calculating A, the variable R is calculated first, using Equation (2-2). The other nuclide parameters given in Table 2-4, the pumped forward parameter given in Table 2-3, and the sample case parameters are used in the equation:

$$R = \frac{1.5 \times 10^5 \times 0.9 + 0.01 \times 15.4 \times 10^6 \times 0.001 \times 0.9}{4.9 \times 10^5} = 0.28$$

Then, using this value of R in Equation (2-4):

$$A = \left(\frac{3758}{4.9 \times 10^5} \right) (110) \left(\frac{0.31 + 4.62 \times 10^{-2}}{0.28 + 4.62 \times 10^{-2}} \right) = 0.92$$

The adjusted concentration of Na-24

$$\begin{aligned} &= (\text{adjustment factor}) \times (\text{standard Na-24 concentration}) \\ &= 0.92 \times 1 \times 10^{-2} \text{ } \mu\text{Ci/gm} = 9.2 \times 10^{-3} \text{ } \mu\text{Ci/gm} \end{aligned}$$

The noble gas concentrations in Table 2-2 are based on an offgas release rate of 50,000 $\mu\text{Ci/sec}$ measured at 30-minute decay. The value of 50,000 $\mu\text{Ci/sec}$ can be determined as discussed below. Recent data supplied by General Electric (Refs. 5,6,7) shows that improved (7 x 7R and 8 x 8) fuel which is in the process of being installed in both new and reload cores has shown considerable improvement over the 7 x 7 fuel which was previously used and still present in some BWRs.

The improvements in the fuel are primarily due to a reduction in zircaloy hydriding and pellet cladding interaction (PCI). However, there is not extensive experience of the improved fuel over complete burnup cycles to date. At the higher burnups, the probability for PCI failure increases even though the power generation rate in the fuel is diminished. This results because at the higher burnups the fuel-to-cladding gap closes due to fission product swelling of the fuel and because the cladding loses its ductility from neutron damage and hydrogen pickup (Ref. 8).

For these reasons, there is not sufficient justification to use the low values of noble gas release rates experienced at reactors having cores loaded with 100% of improved fuel. However, a review was performed of BWR operating experience with noble gas release rates for the period 1975-1977 (Refs. 9, 10) which include the time period during which the improved fuel was introduced. In order to account for the potential effects of increased releases at high burnups and also to account for the fact that the 7 x 7 fuel will be phased out (Ref. 6), only the experience at those reactors whose cores are loaded with greater than 50% of improved fuel was considered. A summary of these data is contained in Table 2-6. Based on this review, the noble gas release rate that will be used as an interim measure until more improved fuel experience is obtained is 50,000 $\mu\text{Ci/sec}$ at 30 minutes decay and normalized to 3400 Mwt.

A carryover factor of 0.015 is used to calculate the halogen concentrations in the main steam in Table 2-2 for BWRs which have deep bed condensate treatment, or for BWRs with powdex filter/demineralizer condensate treatment and having stainless steel condenser tubing. For BWRs with powdex filter/demineralizer condensate treatment systems and copper condenser tubing a carryover factor of 0.004 is used to calculate the halogen concentrations in the main steam. This carryover factor is derived from data taken at operating reactors (Refs. 3, 4, 5, 11 and 12) which are listed in Table 2-7. The average of the data in Table 2-7 is 0.015 and 0.004 for halogen (iodine) carryover, respectively, for the two types of BWRs listed in that table.

The nominal value of the ratio of the condensate demineralizer flow rate to the steam flow rate is 0.75. This indicates that the nominal case is a design which utilizes a pumped forward model, that is, one in which the reactor steam flow is split with 75% flowing to the low pressure turbines and the main condenser, and 25% pumped forward to the feedwater. The fraction pumped forward to the feedwater does not undergo any treatment in the condensate demineralizers. We have determined that the iodine and Cs, Rb, and Other Nuclides of Table 2-2 preferentially go with the "pumped forward" fraction. The reason for this is that these nuclides show a tendency to go with the condensed steam in the moisture separator-reheater drains to the feedwater system. Based on data provided in Ref. 13 and 14 for Brunswick and Point Beach, the ratios used in the BWR-GALE Code are 82% bypass of condensate demineralizers for iodine and 99% bypass of condensate demineralizer for Cs, Rb, and Other Nuclides of Table 2-2. Since the remainder of the nuclides listed in Table 2-2 are not removed in the condensate demineralizers, we have not considered the magnitude of bypass for those nuclides.

TABLE 2-6
 SUMMARY OF NOBLE GAS RELEASE
 RATES FOR OPERATING BWRs*
 (μ Ci/sec)

<u>Facility</u>	<u>1977</u>	<u>1976</u>	<u>1975</u>
Cooper	290	31	-
Dresden 3	215,000	-	-
Duane Arnold	NA	1,300	-
Fitzpatrick	1,190	-	-
Hatch 1	1,300	-	-
Millstone 1	NA	152,000	-
Monticello	91,000	137,000	-
Nine Mile Pt 1	60,000	64,000	-
Oyster Creek	113,000	79,000	-
Peach Bottom 2	12,000	10,000	-
Peach Bottom 3	6,900	-	-
Vermont Yankee	NA	11,000	12,000
	<u>55,000</u>	<u>56,000</u>	<u>12,000</u>

*Data in this table are based on measured noble gas release rates in references 9 and 10 and were adjusted to 30 minutes decay and to 3400 Mwt.

NA - Data not available.

TABLE 2-7
 REACTOR VESSEL HALOGEN CARRYOVER FACTORS
 (PARTITION COEFFICIENTS) OBSERVED AT OPERATING BWRs

BWRs which have Deep Bed Condensate Treatment; BWRs which have Powdex Systems with Stainless Steel Condenser Tubing

BWRs which have Powdex Treatment Systems with Copper Condenser Tubing

<u>Plant</u>	<u>Partition Coefficient</u>	<u>Ref</u>	<u>Plant</u>	<u>Partition Coefficient</u>	<u>Ref</u>
Oyster Creek	0.023	3, 4, 11			
Dresden 2	0.017	3, 12	Monticello	0.004	3
Dresden 3	0.021	3, 12	Browns Ferry 1	0.005	5
Millstone 1	0.012	3, 4	Browns Ferry 2	0.0023	5
Nine Mile Point 1	0.02	4	Browns Ferry 3	0.003	5
Quad Cities 1	0.013	3	Duane Arnold	0.004	5
Cooper	0.012	5	Hatch 1	0.0035	5
Fitzpatrick	0.018	5	Peach Bottom 2	0.004	5
Pilgrim 1	<u>0.0082</u>	5	Peach Bottom 3	0.0044	5
AVERAGE	0.015		Vermont Yankee	<u>0.004</u>	5
			AVERAGE	0.004	

The category "Other nuclides" includes Mo, Y, and Tc which are generally present in colloidal suspensions or as "crud." Although the actual removal mechanism for Y, Mo, and Tc is expected to be plateout or filtration, the quantitative effect of removal is expected to be commensurate with the removal of ionic impurities by ion exchange (within the accuracy of the calculations) and consequently plateout of these nuclides is included in the parameters for ion exchange.

2.2.4 GASEOUS RELEASES FROM BUILDING VENTILATION SYSTEMS

2.2.4.1 Parameter

The noble gas and radioactive particulate releases from ventilation systems for facilities with the BWR/6, Mark III containment design, prior to treatment, are shown in Table 2-12.

The iodine releases from ventilation systems for facilities with the BWR/6, Mark III containment design, prior to treatment, are calculated by the BWR-GALE Code using the data in Table 1-2, Tables 2-2 through 2-5, and 2-8 through 2-10.

2.2.4.2 Bases

The iodine-131 releases from building ventilation systems are based on measurements made at a number of operating reactors. These measurements were made during routine operation and during plant shutdowns. Extensive work on identifying sources of radioiodine at BWRs has been done by C. Pelletier, et al (Ref. 15) for the Electric Power Research Institute (EPRI), at three operating BWRs, Monticello, Vermont Yankee and Oyster Creek, and for the U.S. Nuclear Regulatory Commission at one operating BWR, Pilgrim (Ref. 16).

These measurements indicate that iodine-131 building vent releases are directly related to the reactor water iodine-131 concentration. As a result, the releases of iodine are expressed as "normalized" releases, that is, the absolute measured release rate in $\mu\text{Ci}/\text{sec}$ is divided by the measured reactor water concentration in $\mu\text{Ci}/\text{gm}$ to give a "normalized" release rate of reactor water containing iodine-131 in gm/sec , as shown in the following equation:

$$R_N = \frac{R_A}{C_{RW}}$$

where

R_N = normalized release rate of reactor water containing iodine-131, gm/sec

R_A = absolute (measured) iodine-131 release rate, $\mu\text{Ci}/\text{sec}$

C_{RW} = measured reactor water iodine-131 concentration, $\mu\text{Ci}/\text{gm}$.

The normalized reactor water release rate, expressed in gm/sec , represents an effective leak rate for reactor water containing iodine. It is the combination of the water leakage rate into the building and the effect of iodine partitioning between the water phase in the systems leakage and the vapor phase in the building atmosphere.

For the turbine building, the iodine releases are directly related to the partition coefficient for radioiodine from reactor water to steam, in addition to being directly related to the reactor water iodine-131 concentration. Therefore, for the turbine building, the normalized iodine release, R_N , is determined using the following expression:

$$R_N = \frac{R_A}{C_{RW} \times PC}$$

where

R_N = normalized release rate of reactor water containing iodine-131, gm/sec

R_A = absolute (measured) iodine-131 release rate, $\mu\text{Ci}/\text{sec}$

C_{RW} = measured reactor water iodine-131 concentration, $\mu\text{Ci}/\text{gm}$

PC = measured partition coefficient from the reactor water to reactor steam.

The normalized release rate is used to estimate the releases from BWRs since this expression for release rate is least variable with time and least variable from plant to plant for comparable time periods (Ref. 15). For this reason, it is useful in the determination of releases from BWRs.

Data on the normalized release rates from the three reactors used in the EPRI NP-495 study and the reactor in the NRC study are given for normal operation and shutdown periods in Tables 2-8, 2-9, and 2-10 for the turbine building, the reactor building and the radwaste building, respectively.

Also given in Tables 2-8, 2-9 and 2-10 are normalized values of the iodine release data based on References 3 and 5. The data and the plants included in these references are listed in Tables 2-10 through 2-15 of NUREG-0016, dated April 1976. These data are presented as one data point since the measurements used were of short duration compared to the lengthy measurements carried out in the EPRI NP-495 and the NRC study. Also given in Tables 2-8, 2-9, 2-10 are normalized values of iodine release data from Browns Ferry during 1977 (Ref. 5).

The data in Tables 2-8 through 2-10 are expressed as the total normalized release during power operation of 300 days and the total normalized release during extended shutdown of 65 days. Since the reactors used in the EPRI NP-495 study and the NRC study experienced several intermittent shutdowns of short duration during the power operation measurement period, the iodine releases during these short duration outages are included under power operation.

In order to obtain the releases in curies/yr from the reactor building and radwaste building of a particular BWR, the normalized release data in Tables 2-9 and 2-10, respectively, are multiplied in the BWR-GALE Code by the iodine reactor water concentration for that particular BWR using the following expression:

$$R_{BWR} = R_N^1 \times C_{BWR}$$

where

- R_{BWR} = calculated annual release for particular BWR, Ci/yr
- R_N^1 = normalized annual release of reactor water containing iodine-131 from Tables 2-9 and 2-10, Ci/yr/ μ Ci/gm
- C_{BWR} = calculated reactor water concentration for particular BWR, μ Ci/gm

To obtain the release in curies/yr from the turbine building of a particular BWR, the normalized release data in Table 2-8 are multiplied in the BWR-GALE Code by the iodine reactor water concentration and the iodine carryover from the reactor water to reactor steam for that particular BWR using the following expression:

$$R_{BWR} = R_N^1 \times C_{BWR} \times PC_{BWR}$$

where

- R_{BWR} = calculated annual release for particular BWR, Ci/yr
- R_N^1 = normalized annual release of reactor water from Table 2-8, Ci/yr/ μ Ci/gm
- C_{BWR} = calculated reactor water concentration for particular BWR, μ Ci/gm
- PC_{BWR} = calculated carryover from the reactor water to reactor steam for the particular BWR (See Section 2.2.3.2 and Table 2-4)

The value for the iodine carryover for the reactor water to reactor steam can be determined for the particular BWR from Table 2-4.

To obtain the releases during extended shutdown, multiply the normalized release rates for the extended shutdown period by the same reactor water concentration as for power operation. Use of this reactor water concentration is acceptable since the normalization technique of EPRI-NP-495 based the extended shutdown normalized release rate on the reactor water concentrations prior to shutdown.

The value for the iodine-131 reactor water concentration can be determined as discussed below. Recent data supplied by General Electric (Refs. 5, 6, 7) shows that improved (7 x 7R and 8 x 8) fuel which is in the process of being installed in both new and reload cores has shown considerable improvement over the 7 x 7 fuel which was previously used and still present in some BWRs.

The improvements in the fuel are primarily due to a reduction in zircaloy hydriding and pellet cladding interaction (PCI). However, there is not extensive experience of the improved fuel over complete burnup cycles to date. At the higher burnups, the probability for PCI failure increases even though the power generation rate in the fuel is diminished. This results because at the higher burnups the fuel-to-cladding gap closes due to fission product swelling of the fuel and because the cladding loses its ductility from neutron damage and hydrogen pickup (Ref. 8).

For these reasons, there is not sufficient justification to use the low values of iodine-131 reactor water concentration experienced at reactors having cores loaded with 100% of improved fuel. However, a review was performed of BWR operating experience (Ref. 5) with iodine-131 reactor water concentrations for the period 1975-1977 which includes the time period during which the improved fuel was introduced. In order to account for the potential effects of increased releases at high burnups and also to account for the fact that the 7 x 7 fuel will be phased out (Ref. 6), only the experience at those reactors whose cores are loaded with greater than 50% of improved fuel was considered. A summary of these data is contained in Table 2-11. Based on this review, the iodine-131 reactor water concentration that will be used as an interim measure until more improved fuel experience is obtained is 0.0037 μ Ci/gm.

The reactor building releases reported in References 13 and 14 are based on reactors with a BWR Mark I containment design. Equipment such as the reactor water cleanup (RWCU) pumps, the residual-heat removal system, and emergency core cooling systems have been placed in an auxiliary building in the BWR/6, Mark III containment design concept. Based on data gathered in Reference 15, the RWCU pumps are the major source of leakage in the reactor building. As a result of these measurements, the releases from the Mark III auxiliary building ventilation system are determined to be 90% of Mark I reactor building release, and releases from the Mark III containment building ventilation are determined to be 10% of Mark I releases during power operation. During shutdown, 90% of the releases are determined to be from the Mark III containment building ventilation system and 10% from the auxiliary building ventilation system. For the turbine building, based on data gathered in Ref. 15, 85% of the releases are determined to come from the ventilation system serving the main condenser area during power operation. The remainder of the releases come from miscellaneous areas such as the steam jet air ejector room, the turbine operating floor, the feedwater pump room, and the mechanical vacuum pump room. During the shutdown since there is potential for iodine release during maintenance of the turbines, the release from the ventilation system serving the main condenser area is approximately 50% of the total and the remainder of the releases come from the miscellaneous areas.

For the radwaste building, based on data gathered in Ref. 15, 10% of the releases are determined to come from the solid waste handling area and 90% of the releases are determined to come from the liquid waste handling area.

Within the building ventilation systems, charcoal adsorbers may be added on individual equipment cells and appropriate credit taken for iodine removal if the fraction of total iodine being assigned to that particular equipment cell is in accordance with Ref. 15.

Iodine released from BWR building ventilation systems appear in one of the following chemical forms: particulate, elemental, hypoiodous acid (HOI) and organic. Based on data in References 15 and 16 the fraction of the iodine appearing in each of the chemical forms for each building ventilation system is given below:

FRACTION OF IODINE APPEARING IN EACH CHEMICAL FORM
FROM BWR BUILDING VENTILATION SYSTEMS

	<u>CONTAINMENT</u>	<u>AUXILIARY</u>	<u>TURBINE</u>	<u>RADWASTE</u>
Particulate	0.11	0.2	0.2	0.002
Elemental	0.32	0.48	0.50	0.28
HOI	0.38	0.24	0.22	0.25
Organic	0.19	0.09	0.08	0.47

TABLE 2-8
ANNUAL IODINE NORMALIZED RELEASES*
FROM TURBINE BUILDING VENTILATION SYSTEMS

NORMAL OPERATION

<u>Data Source</u>	<u>Normalized Release (Ci/yr/μCi/gm)</u>
Monticello (Ref. 15)	3.1×10^3
Oyster Creek (Refs. 15, 16)	6.0×10^3
Vermont Yankee (Ref. 15)	0.35×10^3
Pilgrim (Ref. 16)	8.5×10^3
Browns Ferry (Ref. 5)	1.3×10^3
References 3 and 5***	3.3×10^3
AVERAGE	3.8×10^3

EXTENDED SHUTDOWN

<u>Data Source</u>	<u>Normalized Release (Ci/yr/μCi/gm)</u>
Monticello (Ref. 15)	1.7×10^2
Oyster Creek (Ref. 15)	$3.5 \times 10^{2**}$
Vermont Yankee (Ref. 15)	0.63×10^2
Browns Ferry (Ref. 5)	1.3×10^2
References 3 and 5***	1.4×10^3
AVERAGE	$4.1 \times 10^{2**}$

*The normalized release rate, expressed in grams of water during the modes of operation, represents the effective leak rate for radioiodine. It is the combination of the reactor water leakage rate into the buildings, the partitioning of the radioiodine between the water phase in the leakage and the gas phase where it is measured and the partition coefficient for radioiodine from reactor water to steam in the reactor vessel.

**Oyster Creek data in this table does not include effect of use of reheater protection system exhaust since the system design of this component is not typical of current BWRs (Nine Mile Point, Unit No. 1 is the only other BWR with this design). If a BWR uses this design, the additional release is 8.7×10^2 Ci/yr/ μ Ci/gm during the shutdown period (Ref. 15) and should be included in the total turbine building shutdown release.

***The data and the plants included in these references are listed in Tables 2-10 through 2-15 of NUREG-0016, dated April 1976.

TABLE 2-9
ANNUAL IODINE NORMALIZED RELEASES*
FROM REACTOR BUILDING VENTILATION SYSTEMS

NORMAL OPERATION

<u>Data Source</u>	<u>Normalized Releases</u> (Ci/yr/ μ Ci/gm)
Monticello (Ref. 15)	11
Pilgrim (Ref. 16)	13
Brown Ferry (Ref. 5)	4.2
References 3 and 5***	<u>21</u>
	12.3**

EXTENDED SHUTDOWN

<u>Data Source</u>	<u>Normalized Releases</u> (Ci/yr/ μ Ci/gm)
Monticello (Ref. 15)	0.47
Oyster Creek (Ref. 15)	1.3
Vermont Yankee (Ref. 15)	3.2
Browns Ferry (Ref. 5)	1.4
References 3 and 5***	<u>20</u>
	5.2

* The normalized release rate, expressed in grams of water during the modes of operation, represents the effective leak rate for radioiodine. It is the combination of the reactor water leakage rate into the buildings, and the partitioning of the radiiodine between the water phase in the leakage and the gas phase where it is measured.

**Oyster Creek and Vermont Yankee data are not included here since Monticello leakage is considered to be more typical of similar problems at other BWRs where the RWCU pump is upstream of the RWCU demineralizers.

*** The data and the plants included in these references are listed in Tables 2-10 through 2-15 of NUREG-0016, dated April 1976.

TABLE 2-10
ANNUAL IODINE NORMALIZED RELEASES*
FROM RADWASTE BUILDING VENTILATION SYSTEMS

NORMAL OPERATION

<u>Data Source</u>	<u>Normalized Release (Ci/yr/μCi/gm)</u>
Monticello (Ref. 15)	0.72
Oyster Creek (Refs. 15, 16)	6.8
Vermont Yankee (Ref. 15)	1.0
Pilgrim (Ref. 16)	12
Browns Ferry (Ref. 5)	2.0
References 3 and 5**	<u>5.3</u>
AVERAGE	4.6

EXTENDED SHUTDOWN

<u>Data Source</u>	<u>Normalized Release (Ci/yr/μCi/gm)</u>
Monticello (Ref. 15)	0.02
Oyster Creek (Ref. 15)	1.4
Vermont Yankee (Ref. 15)	0.4
Browns Ferry (Ref. 5)	0.6
References 3 and 5**	<u>4.4</u>
AVERAGE	1.4

*The normalized release rate, expressed in grams of water during the modes of operation, represents the effective leak rate for radioiodine. It is the combination of the reactor water leakage rate into the buildings, and the partitioning of the radiodine between the water phase in the leakage and the gas phase where it is measured.

**The data and the plants included in these references are listed in Tables 2-10 through 2-15 of NUREG-0016, dated April 1976.

TABLE 2-11
SUMMARY OF IODINE-131 REACTOR WATER
CONCENTRATIONS IN BWR'S*
($\mu\text{Ci/Kg}$)

<u>Facility</u>	<u>1977</u>	<u>1976</u>	<u>1975</u>
Browns Ferry 1	0.9	-	-
Browns Ferry 2	1.5	-	-
Browns Ferry 3	0.14	-	-
Brunswick 1	0.02	-	-
Brunswick 2	3.1	0.93	0.007
Cooper	0.072	0.09	0.013
Dresden 3	17.6	12.6	-
Duane Arnold	0.042	0.09	0.0023
Fitzpatrick	0.24	0.29	-
Hatch 1	0.9	0.11	-
Millstone Pt. 1	8.9	5.6	7.1
Monticello	5.9	9.0	8.7
Nine Mile Pt. 1	9.4	5.9	-
Oyster Creek	8.4	5.3	4.8
Peach Bottom 2	7.3	16.	0.045
Peach Bottom 3	1.1	0.83	0.063
Quad Cities 1	3.4	-	-
Vermont Yankee	<u>0.38</u>	<u>0.51</u>	<u>0.78</u>
	3.8	4.4	2.4

*Data in these tables are based on measured iodine-131 coolant concentrations in Ref. 5 and have been adjusted to the NSSS parameters listed in Table 2-3 of this report. These adjustments were made by considering the individual plant parameters and the nominal plant parameters (Table 2-3) and adjusting the actual coolant concentration using the equations in Table 2-5 of this report.

TABLE 2-12
GASEOUS AND PARTICULATE RELEASES FROM
BUILDING VENTILATION SYSTEMS
(in Ci/yr per Reactor)

<u>NUCLIDE</u>	<u>CONTAINMENT BUILDING</u>	<u>AUXILIARY BUILDING</u>	<u>TURBINE BUILDING</u>	<u>RADWASTE BUILDING</u>
Kr83m	**	**	**	**
Kr-85m	1	3	25	**
Kr-85	**	**	**	**
Kr-87	**	2	61	**
Kr-88	1	3	91	**
Kr-89	**	2	580	29
Xe-131m	**	**	**	**
Xe-133m	**	**	**	**
Xe-133	27	83	150	220
Xe-135m	15	45	400	530
Xe-135	33	94	330	280
Xe-137	45	135	1000	83
Xe-138	2	6	1000	2
Cr-51*	0.0002	0.0009	0.0009	0.0007
Mn-54	0.0004	0.001	0.0006	0.004
Fe-59	0.00009	0.0003	0.0001	0.0003
Co-58	0.0001	0.0002	0.001	0.0002
Co-60	0.001	0.004	0.001	0.007
Zn-65	0.001	0.004	0.006	0.0003
Sr-89	0.00003	0.00002	0.006	NA
Sr-90	0.000003	0.000007	0.00002	NA
Zr-95	0.0003	0.0007	0.00004	0.0008
Nb-95	0.001	0.009	0.000006	0.000004
Mo-99	0.006	0.06	0.002	0.000003
Ru-103	0.0002	0.004	0.00005	0.000001
Ag-110	0.0000004	0.000002	NA	NA
Sb-124	0.00002	0.00003	0.0001	0.00007
Cs-134	0.0007	0.004	0.0002	0.0024
Cs-136	0.0001	0.0004	0.0001	NA
Cs-137	0.001	0.005	0.001	0.004
Ba-140	0.002	0.02	0.010	0.000004
Ce-141	0.0002	0.0007	0.010	0.000007

*Particulate release rates are prior to filtration.

**Less than 1 Ci/yr per reactor.

NA Not Analyzed; analysis for the isotope was not performed.

TABLE 2-13
RELEASE RATES OF NOBLE GASES FROM
THE REACTOR BUILDING VENTILATION SYSTEM
 ($\mu\text{Ci}/\text{sec}$)

<u>NUCLIDE</u>	<u>MILLSTONE-1</u>	<u>OYSTER CREEK</u>	<u>OYSTER CREEK</u>	<u>MONTICELLO</u>	<u>AVERAGE</u>
Kr-85m	0.26	ND	ND	0.20	0.12
Kr-87	0.24	ND	ND	0.10	0.085
Kr-88	0.38	0.02	ND	0.20	0.15
Kr-89	ND	ND	ND	0.38	0.095
Xe-133	0.52	15	ND	2.0	4.4
Xe-135m	3.6	ND	2.5	3.5	2.4
Xe-135	3.0	2.1	14	1.8	5.2
Xe-137	ND	ND	ND	30	7.5
Xe-138	0.44	0.3	ND	0.4	0.29

ND - Not Detected. For averaging purposes a value of zero was assumed.

TABLE 2-14
RELEASE RATES OF NOBLE GASES FROM
THE TURBINE BUILDING VENTILATION SYSTEM
 ($\mu\text{Ci}/\text{sec}$)

<u>NUCLIDE</u>	<u>MILLSTONE-1</u>	<u>OYSTER CREEK</u>	<u>OYSTER CREEK</u>	<u>MONTICELLO</u>	<u>NINE MILE PT 1</u>	<u>AVERAGE</u>
Kr-85m	2.7	ND	2.3	0.10	0.097	1.0
Kr-87	5.3	ND	6.2	0.15	0.53	2.4
Kr-88	8.2	5.2	4.2	0.065	0.21	3.6
Kr-89	ND	ND	70	42	4.5	23
Xe-133	7.4	13	ND	5.0	3.5	5.8
Xe-135m	29	12	26	8.2	2.5	16
Xe-135	25	25	7.4	6.8	2.3	13
Xe-137	ND	ND	115	86	ND	40
Xe-138	63	26	97	11	4.3	40

ND - Not Detected. For averaging purposes a value of zero was assumed.

TABLE 2-15

RELEASE RATES OF NOBLE GASES FROM
 THE RADWASTE BUILDING VENTILATION SYSTEM
 ($\mu\text{Ci}/\text{sec}$)

<u>NUCLIDE</u>	<u>MILLSTONE-1</u>	<u>OYSTER CREEK</u>	<u>MONTICELLO</u>	<u>AVERAGE</u>
Kr-89	ND	ND	3.0	1.0
Xe-133m	ND	ND	5.3	1.8
Xe-133	0.25	0.56	26	8.9
Xe-135m	ND	4	59	21
Xe-135	2.0	1.5	20	7.8
Xe-137	ND	ND	10	3.3
Xe-138	ND	ND	0.2	0.067

ND - Not Detected. For averaging purposes a value of zero was assumed.

TABLE 2-16

PARTICULATE RELEASE RATES FROM REACTOR BUILDING
 VENTILATION SYSTEM, NORMAL OPERATION
 ($10^{-6} \mu\text{Ci}/\text{sec}$)

<u>NUCLIDE</u>	<u>QUAD CITIES 1</u>	<u>QUAD CITIES 2</u>	<u>VERMONT YANKEE</u>	<u>OYSTER CREEK</u>	<u>MONTICELLO</u>	<u>AVERAGE</u>
Co-60	210	0.9	37	610	140	200
Co-58	20	0.4	5.5	31	ND	11
Cr-51	140	0.5	13	39	ND	38
Mn-54	19	0.1	14	210	24	53
Fe-59	NA	NA	5	33	4.2	14
Zn-65	23	0.1	46	6.4	750	160
Sr-89	NA	NA	NA	6.8	NA	6.8
Sr-90	NA	NA	NA	0.3	NA	0.3
Zr-95	1.6	ND	1.5	0.5	115	24
Nb-95	2.7	ND	7.4	0.3	2200	440
Mo-99	NA	NA	4.4	140	7300	2500
Ru-103	NA	NA	ND	2.8	65	23
Ag-110m	0.2	ND	NA	NA	NA	0.1
Sb-124	NA	NA	ND	2.4	ND	0.8
Cs-134	48	0.1	12	16	760	170
Cs-136	2.3	ND	6.8	7.1	79	19
Cs-137	44	0.5	37	31	990	220
Ba-140	ND	ND	16	76	2600	540
Ce-141	NA	ND	ND	3.9	120	31

NA - Not Analyzed.

ND - Not Detected. For averaging purposes a value of zero was assumed.

The noble gas release rates for building ventilation systems are the average of measurements made at Oyster Creek (Ref 17), Millstone Unit No. 1 (Ref. 18), Monticello (Ref. 15), and Nine Mile Point (Ref. 19). These data are given in Tables 2-13 through 2-15 and are based on the fuel handling area being in the containment building. The noble gas release rates are divided between the containment and auxiliary buildings to reflect the BWR/6, Mark III design, in a manner similar to that for the iodine-131 release.

For the Mark III design during shutdown, 90% of the releases are assumed to be from the containment building and 10% from the auxiliary building ventilation system since the releases from the fuel handling area are considered to be the major source. For the BWR/6 Mark-III containment system design, the fuel building releases are considered to be part of the containment building releases.

The radioactive particulate release rates for building ventilation systems are the average of measurements made at Vermont Yankee, Oyster Creek, Dresden 2 & 3, Quad Cities 1 & 2, Monticello, and Nine Mile Point (Refs. 3, 5, 15 and 19). These data are given in Tables 2-16 through 2-21.

The calculated annual average rates given above are based on an 80% plant capacity factor, i.e., 80% normal operation at 100% power and 20% plant downtime. The releases for normal operation are weighted to account for the operating and shutdown modes. The particulate releases for the reactor building are divided between the containment and auxiliary buildings to reflect the BWR/6, Mark III containment design in a manner similar to that for the iodine-131 releases.

2.2.5 IODINE INPUT TO THE MAIN CONDENSER OFFGAS TREATMENT SYSTEM

2.2.5.1 Parameter

The iodine-131 input to the main condenser offgas treatment system, downstream of the air ejectors, is 6 Ci/yr.

2.2.5.2 Bases

Table 2-22 lists the measured iodine-131 releases and integrated thermal power outputs for BWRs with thermal ratings exceeding 1000 MWt, with more than one year of plant operation and without main condenser offgas treatment. The average ratio of the iodine-131 release in Ci/yr to the integrated thermal power in MWd for the years 1972 through 1976 is approximately 6.3×10^{-6} Ci/MWd per year. Based on a power rating of 3400 MWt and an 80% plant capacity factor, the iodine-131 release from the main condenser air ejector is approximately 6 Ci/yr.

2.2.6 TURBINE GLAND SEALING SYSTEM EXHAUST

2.2.6.1 Parameter

If main steam is used, the annual radioiodine releases from the gland seal condenser exhaust are:

$$\begin{aligned} \text{I-131} &= 8.1 \times 10^{-1} \text{ Ci/yr per } \mu\text{Ci/gm of I-131 in the reactor coolant.} \\ \text{I-133} &= 2.2 \times 10^{-1} \text{ Ci/yr per } \mu\text{Ci/gm of I-133 in the reactor coolant.} \end{aligned}$$

If the clean steam is supplied to the gland seal, the radioiodine source term is negligible (less than 10^{-4} Ci/yr). If sealing steam is supplied from a low-activity source, i.e., steam produced from demineralized condensate, consider the release to be zero.

2.2.6.2 Bases

Radioiodine measurements have been reported (Ref. 15) for two operating facilities that use main steam in the turbine gland seal system. The sample location necessitated including any radioiodines released from the mechanical vacuum pump during sampling. Table 2-23 summarizes this available data for radioiodines released from the gland seal condenser exhaust when the mechanical vacuum pump was not in operation or infrequently used. The radioiodine release rates are dependent on the radioiodine concentration in the reactor coolant and carry-over in the reactor.

It is assumed that there is no radioiodine source term when clean steam (non-radioactive steam from an auxiliary steam supply system) is used for the gland seal. Because of noble gas removal in the main steam condenser, radioiodine removal by the condensate demineralizers, and partitioning in the boiler, steam produced from demineralized condensate is considered to be clean steam. Data in Tables 2-24 and 2-25 show the release of radioactive particulates from the turbine gland seal to be negligible (less than 10^{-5} Ci/year).

TABLE 2-17

PARTICULATE RELEASE RATES FROM REACTOR BUILDING
VENTILATION SYSTEM, REFUELING SHUTDOWN

$(10^{-6} \mu\text{Ci/sec})$

NUCLIDE	QUAD CITIES 1	QUAD CITIES 2	VERMONT YANKEE	OYSTER CREEK	MONTICELLO	AVERAGE
Co-60	16	0.88	250	330	1.70	120
Co-58	2.3	0.35	41	19	ND	13
Cr-51	8.9	0.50	63	28	ND	20
Mn-54	2.6	0.061	20	140	47	42
Fe-59	ND	ND	21	5.0	3.4	6.0
Zn-65	58	0.11	770	1.4	73	180
Sr-89	NA	NA	NA	2.0	NA	2.0
Sr-90	NA	NA	NA	0.36	NA	0.36
Zr-95	0.31	ND	78	0.24	ND	16
Nb-95	0.40	0.021	ND	0.41	160	32
Mo-99	NA	NA	ND	13	4.4	5.8
Ru-103	NA	NA	NA	1.3	36	19
Ag-110m	0.11	NA	NA	NA	NA	0.11
Sb-124	ND	ND	NA	7.0	ND	1.8
Cs-134	6.2	0.14	82	13	170	54
Cs-136	1.0	NA	20	ND	21	11
Cs-137	14	0.54	240	23	200	95
Ba-140	ND	ND	14	1.1	200	43
Ce-141	ND	ND	NA	7.5	45	13

NA - Not Analyzed.

ND - Not Detected. For averaging purposes a value of zero was assumed.

TABLE 2-18

PARTICULATE RELEASE RATES FROM TURBINE BUILDING
VENTILATION SYSTEM, NORMAL OPERATION

$(10^{-6} \mu\text{Ci/sec})$

NUCLIDE	OYSTER CREEK	MONTICELLO	VERMONT YANKEE	DRESDEN 2	DRESDEN 3	AVERAGE
Co-60	61	15	4.1	4.5	6.0	18
Co-58	12	ND	2.0	ND	48	12
Cr-51	440	ND	NA	ND	160	150
Mn-54	30	7.5	1.9	ND	5	8.9
Fe-59	5.8	ND	ND	ND	ND	1.2
Zn-65	1.7	23	7.8	ND	ND	6.5
Sr-89	610	NA	NA	48	3.6	220
Sr-90	1.3	NA	NA	0.3	0.25	0.6
Zr-95	0.59	ND	ND	ND	4.0	0.92
Nb-95	0.33	ND	NA	ND	ND	0.1
Mo-99	91	150	NA	ND	ND	61
Ru-103	1.7	ND	ND	ND	ND	0.34
Sb-124	4.6	ND	ND	ND	ND	0.92
Cs-134	18	23	2.7	ND	3.0	9.3
Cs-136	1.1	16	ND	ND	ND	3.4
Cs-137	57	100	5.1	1.8	10	35
Ba-140	1400	16	83	120	65	340
Ce-141	29	1600	ND	5.5	5	328

NA - Not Analyzed.

ND - Not Detected. For averaging purposes a value of zero was assumed.

TABLE 2-19
PARTICULATE RELEASE RATES FROM TURBINE BUILDING
VENTILATION SYSTEM, REFUELING SHUTDOWN
 (10⁻⁶ μ Ci/sec)

<u>NUCLIDE</u>	<u>OYSTER CREEK</u>	<u>VERMONT YANKEE</u>	<u>MONTICELLO</u>	<u>AVERAGE</u>
Co-60	290	2.5	5.8	100
Co-58	16	1	NA	8.5
Cr-51	51	ND	NA	26
Mn-54	110	NA	0.30	57
Fe-59	31	ND	ND	10
Zn-65	11	NA	10	10
Sr-89	2.5	NA	NA	2.5
Sr-90	0.25	NA	NA	0.25
Zr-95	0.06	ND	ND	0.02
Nb-95	0.40	ND	ND	0.13
Mo-99	125	NA	9.7	67
Ru-103	5.2	NA	ND	2.6
Sb-124	9.5	ND	NA	4.8
Cs-134	19	1.9	1.3	7.4
Cs-136	ND	ND	4.1	1.4
Cs-137	39	3.4	5.8	16
Ba-140	8.2	110	49	56
Ce-141	17	ND	9.1	8.7

NA - Not Analyzed.
 ND - Not Detected. For averaging purposes a value of zero was assumed.

TABLE 2-20
PARTICULATE RELEASE RATE FROM RADWASTE BUILDING
VENTILATION SYSTEM, NORMAL OPERATION
 (10⁻⁶ μ Ci/sec)

<u>NUCLIDE</u>	<u>VERMONT YANKEE</u>	<u>OYSTER CREEK</u>	<u>AVERAGE</u>
Co-60	6.0	580	290
Co-58	1.0	16	8
Cr-51	3.0	48	26
Mn-54	1.0	330	170
Fe-59	ND	26	13
Zn-65	1.0	21	11
Sr-89	NA	NA	NA
Sr-90	NA	NA	NA
Zr-95	ND	63	31
Mo-99	2.0	ND	1.0
Sb-124	ND	5.4	2.7
Cs-134	1.2	190	96
Cs-136	ND	ND	0
Cs-137	2.0	290	150
Ba-140	0.3	ND	0.15
Ce-141	ND	6.3	3.2

NA - Not Analyzed
 ND - Not Detected. For averaging purposes a value of zero was assumed.

TABLE 2-21
 PARTICULATE RELEASE RATE FROM RADWASTE BUILDING
 VENTILATION SYSTEM, REFUELING SHUTDOWN
 (10⁻⁶ μ Ci/sec)

<u>NUCLIDE</u>	<u>MONTICELLO</u>	<u>AVERAGE</u>
Co-60	1.3	1.3
Co-58	0.21	0.21
Cr-51	ND	0
Mn-54	0.40	0.40
Fe-59	3.2	3.2
Zn-65	5.1	5.1
Sr-89	NA	NA
Sr-90	NA	NA
Nb-95	6.0	6.0
Mo-99	1.0	1.0
Ru-103	1.0	1.0
Ru-103	1.0	1.0
Sb-124	ND	0
Cs-134	1.0	1.0
Cs-136	ND	0
Cs-137	2.2	2.2
Ba-140	ND	0
Ce-141	1.2	1.2
Ce-144	4.0	4.0

NA - Not Analyzed.

ND - Not Detected. For averaging purposes a value of zero was assumed.

TABLE 2-22
RADIOIODINE-131 RELEASES FROM THE MAIN CONDENSER AIR EJECTORS^a

FACILITY	1972		1973		1974	
	RADIO- IODINE RELEASE (Ci/yr)	INTEGRATED THERMAL POWER (10 ⁶ Mwd) Ci/yr 10 ⁶ Mwd	RADIO- IODINE RELEASE (Ci/yr)	INTEGRATED THERMAL POWER (10 ⁶ Mwd) Ci/yr 10 ⁶ Mwd	RADIO- IODINE RELEASE (Ci/yr)	INTEGRATED THERMAL POWER (10 ⁶ Mwd) Ci/yr 10 ⁶ Mwd
Oyster Creek	6.3	0.542	6.7	0.453	3.3	0.46
Nine Mile Point 1	0.89	0.417	1.9	0.457	0.7	0.43
Millstone 1	1.2	0.404	0.15	0.248	0.29	0.47
Dresden 2/3 ^b	5.1	1.05	9.8	1.18	4.0	0.91
Monticello	0.58	0.454	1.2	0.413	5.7	0.34
Pilgrim 1		c	0.46	0.523	1.4	0.25
Quad Cities 1/2 ^b		c	5.5	1.32	8.2	1.09
Average		4.6				
						5.1
						6.2

Combined average for 1972 through 1976 = 6.3×10^{-6} Ci/yr
Mwd

^aData from semiannual operating for 1972 through 1976 for facilities listed.
^bTwo-unit plants with a single stack.
^cNot included in 1972 average because plants had not achieved a full year of operation.
^dAugmented offgas system put in operation October 1975.
^eAugmented offgas system put in operation late 1976.
^fAugmented offgas system put in operation May 1975.
^gAugmented offgas system put into operation 1977.
^hAugmented offgas system put into operation late 1974.

TABLE 2-22 (continued)

RADIOIODINE-131 RELEASES FROM THE MAIN CONDENSER AIR EJECTORS

FACILITY	1975			1976		
	RADIO- IODINE RELEASE (Ci/yr)	INTEGRATED THERMAL POWER (10 ⁶ MWd)	Ci/yr 10 ⁶ MWd	RADIO- IODINE RELEASE (Ci/yr)	INTEGRATED THERMAL POWER (10 ⁶ MWd)	Ci/yr 10 ⁶ MWd
Oyster Creek	5.5	0.41	13.4	6.2	0.49	12.7
Nine Mile Point 1	2.1	0.4	5.3	2.1	0.55	3.8 ^g
Millstone 1	9.8	0.5	19.6	2.7	0.48	5.6
Dresden 2/3 ^b	0.75	0.71	1.06	1.9	1.14	1.7 ^e
Monticello	3.5	0.37	9.5	d		
Pilgrim 1	h					
Quad Cities 1/2 ^b	f					
Average			9.8			6.0

TABLE 2-23

RADIOIODINE RELEASE RATE FROM GLAND SEAL CONDENSER EXHAUST
FOR SYSTEMS USING MAIN STEAM FOR THE SEALING SYSTEM AT 7000 lbs/hr.

Nuclide	Facility	Sample Period	Days	Measured Gland Seal I-131 Release ($\mu\text{Ci}/\text{sec}$)	Measured Reactor Water I-131 Concentration ($\mu\text{Ci}/\text{gm}$)	Iodine-131 Release Ci/yr per Ci/gm for 292 days/year
I-131	Vermont Yankee	6/18/74 to 6/19/74	1	3.9(-4)	2.5(-2)	3.9(5)
		6/20/74 to 6/21/74	1	4.2(-4)	2.5(-2)	4.2(5)
		9/13/74 to 9/14/74	1	4.7(-4)	3.8(-2)	3.1(5)
		10/10/74 to 10/11/74	1	4.5(-4)	3.5(-2)	3.2(5)
		3/5/75 to 3/8/75	3	2.1(-5)	8.8(-4)	6.0(5)
		10/7/75 to 10/21/74	14	1.4(-5)	7.7(-4)	4.6(5)
Oyster Creek		6/16/75 to 6/30/75	14	7.8(-5)	1.8(-3)	1.1(6)
		6/30/75 to 7/17/75	17	6.8(-5)	1.7(-3)	1.0(6)
Weighted Average According to Sample Days						
						8.1(5)
Nuclide	Facility	Sample Period	Days	Measured Gland Seal I-133 Releases ($\mu\text{Ci}/\text{sec}$)	Measured Reactor Water I-133 Concentration ($\mu\text{Ci}/\text{gm}$)	Parameter (Ci/yr per Ci/gm) for 292 days/year
I-133	Vermont Yankee	6/18/74 to 6/19/74	1	1.8(-4)	5.6(-2)	8.1(4)
		6/20/74 to 6/21/74	1	1.9(-4)	5.6(-2)	8.6(4)
		9/13/74 to 9/14/74	1	2.2(-4)	1.1(-2)	5.0(5)
		10/10/74 to 10/11/74	1	1.7(-4)	1.0(-2)	4.3(5)
		6/16/75 to 6/30/75	14	2.3(-4)	2.6(-2)	2.2(5)
Oyster Creek		6/30/75 to 7/17/75	17	2.0(-4)	2.4(-2)	2.1(5)
Weighted Average According to Sample Days						
						2.2(5)

TABLE 2-24

PARTICULATE RELEASE RATE FROM VERMONT YANKEE MECHANICAL
VACUUM PUMP AND GLAND EXHAUST CONDENSER VENT,
SHORT-TERM SHUTDOWN

(10^{-6} μ Ci/sec)

<u>NUCLIDE</u>	<u>RELEASE RATE</u>
Cr-51	0.9
Co-60	0.5
Zn-65	0.3
Cs-134	0.8
Cs-136	1.1
Cs-137	3.3
Ba-140	2.1

TABLE 2-25

PARTICULATE RELEASE RATE FROM VERMONT YANKEE MECHANICAL
VACUUM PUMP AND GLAND EXHAUST CONDENSER VENT,
REFUELING SHUTDOWN

(10^{-6} μ Ci/sec)

<u>NUCLIDE</u>	<u>RELEASE RATE</u>
Cs-134	0.45
Cs-136	0.13
Cs-137	1.0
Ba-140	1.6

TABLE 2-26

NORMALIZED IODINE RELEASES FROM
MECHANICAL VACUUM PUMP
(\leq 80 HRS)

<u>Plant</u>	<u>Normalized Release</u> (Ci/yr/ μ Ci/gm)
Monticello	8.3(2)
Vermont Yankee	<u>1.5(2)</u>
AVERAGE	4.9(2)

NORMALIZED IODINE RELEASES FROM
MECHANICAL VACUUM PUMP DURING REFUELING/MAINTENANCE
OUTAGES (\geq 80 HRS)

<u>Plant</u>	<u>Normalized Release</u> (Ci/yr/ μ Ci/gm)
Monticello	1.5(3)
Vermont Yankee	<u>6.0(2)</u>
AVERAGE	1.1(3)

^{1/}Assume (4) short-term outages per year.

2.2.7 MAIN CONDENSER MECHANICAL VACUUM PUMP

2.2.7.1 Parameter

Xe-133	1300 Ci/yr per reactor
Xe-135	500 Ci/yr per reactor

The iodine releases from the Main Condenser Mechanical Vacuum Pump are calculated by the BWR-GALE Code using the data in Tables 2-2, 2-4 and 2-26.

2.2.7.2 Bases

The release rates for Xe-133 and Xe-135 were derived from Dresden 1 and 2 operating data and adjusted to 50,000 $\mu\text{Ci/sec}$ (Ref. 5). These data indicate that approximately 300 Ci of Xe-133 and 120 Ci of Xe-135 were released with the mechanical vacuum pump effluent when the main condenser vacuum pumps were used to establish main condenser vacuum following a plant shutdown. At the point in the fuel cycle where the data were taken, the reactor was operating at an offgas rate of approximately 60,000 $\mu\text{Ci/sec}$. The annual release estimates for noble gases assumes four short-term shutdowns per year and one refueling/maintenance outage.

The release rates for iodine-131 are based on measurements made at operating reactors (Ref. 15). Investigations for the Electric Power Research Institute (EPRI) at three operating Boiling Water Reactors (BWRs), Monticello, Vermont Yankee, and Oyster Creek, have shown that iodine releases from the mechanical vacuum pump are at their highest levels for the first 80 hours after shutdown. In accordance with the EPRI study, the releases from the mechanical vacuum pump can be as much as a factor of 100 greater than releases measured during the pre-shutdown period. The normalized iodine-131 releases in Table 2-26 are based on data from Monticello and Vermont Yankee.

The annual iodine-131 release estimates assume four short term shutdowns per year and one refueling/maintenance outage per year.

To calculate releases from the mechanical vacuum pump, a normalized release rate is used. The normalized release rate is calculated by the BWR-GALE Code using the following expression:

$$R_N = \frac{R_A}{C_{RW} \times PC}$$

where

- R_N = normalized release rate of reactor water containing iodine-131, (gm/sec)
- R_A = absolute (measured) iodine-131 release rate, ($\mu\text{Ci/sec}$)
- C_{RW} = measured reactor water iodine-131 concentration, ($\mu\text{Ci/gm}$)
- PC = measured partition coefficient from reactor water to reactor steam.

To calculate the release in Ci/yr from the mechanical vacuum pump of a particular BWR, the normalized release data in Table 2-26 are multiplied by the iodine reactor water concentration and the iodine carryover from reactor water to reactor steam for the particular BWR using the following expression:

$$R_{MVP} = R_N' \times C_{BWR} \times PC_{BWR}$$

where:

- R_N' = normalized release rate of reactor water containing iodine-131, (Ci/yr/ $\mu\text{Ci/gm}$)
- R_{MVP} = calculated annual iodine release, (Ci/yr) from the mechanical vacuum pump
- C_{BWR} = reactor water concentration for a particular BWR, ($\mu\text{Ci/gm}$)
- PC_{BWR} = calculated carryover for particular BWR from Table 2-4.

Iodine released during the operation of the Mechanical Vacuum Pump at BWRs appear in one of the following chemical forms: particulate, elemental, hypoiodous acid (HOI), and organic. Based on data in Reference 15, the fraction of the iodine appearing in each of the chemical forms for the Mechanical Vacuum Pump is given below:

Fraction of Iodine Appearing In Each Chemical Form From
BWR Mechanical Vacuum Pump

	<u>Time < 80 hrs^{1/}</u>	<u>Time > 80 hrs^{2/}</u>
Particulate	0.004	0.01
Elemental	0.009	0.06
HOI	0.023	0.21
Organic	0.97	0.72

^{1/}Average of samples taken within the first 80 hrs after shutdown.

^{2/}Average of samples taken after the initial 80 hrs of a refueling maintenance outage.

Data in Tables 2-24 and 2-25 show the release of radioactive particulates from the mechanical vacuum pump to be negligible.

2.2.8 AIR INLEAKAGE TO THE MAIN CONDENSER

2.2.8.1 Parameter

0.0062 ft³/min air leakage to the main condenser per Mwt of design reactor power with a minimum of 5 ft³/min.

2.2.8.2 Bases

Air leakage occurs in the main condensers of all power reactors. In a BWR, the amount of holdup time calculated for a charcoal bed offgas delay system is inversely proportional to the amount of air leakage to the main condenser.

Operational data for leakage vary widely. At Oyster Creek and at Dresden Unit No. 2, air leakage measurements during early phases of operation indicated leakage rates from 4 ft³/min to 250 ft³/min. (Refs. 21₃ and 22). Subsequent measurements at Dresden Unit 2 (Ref. 20), showed an air leakage of 4.4 ft³/min during operation at 1600 Mwt. Air leakage measurements reported for six TVA fossil plants, representing more than 50 years of cumulative experience, indicate leakage rates ranging from 4 to 25 ft³/min per condenser shell and a statistical mean leakage rate of 6.7 ft³/min per condenser shell (Ref. 23). Measurements made in 1976 and 1977, at Quad Cities Units Nos. 1 and 2 (Ref. 24), showed average flow rates of 9.6 ft³/min for Unit No. 1 and 25 ft³/min for Unit No. 2; measurements ranged from 6 ft³/min to 55 ft³/min and power level for both units during the test period was 2511 Mwt.

The parameter for air leakage was developed assuming that air leakage is proportional to the reactor design thermal power level. Available data, which were considered to represent long-term operational results, were converted by extrapolation to the common base of a 3400 Mwt BWR with a 3 shell condenser. The use of data from Dresden Unit No. 2, Quad Cities Unit Nos. 1 and 2, and TVA fossil plants resulted in an average of 21 ft³/min main condenser air leakage for a plant with a design thermal power level of 3400 Mwt. This is approximately equivalent to 0.0062 ft³/min leakage for each Mwt of design thermal power. For BWRs of less than 800 Mwt design thermal power level, a minimum condenser air leakage of 5 ft³/min should be used, independent of reactor design thermal power level.

CONDENSER AIR INLEAKAGE

<u>Plant</u>	<u>Power Level</u>	<u>Reported Data</u>	<u>Extrapolated to 3400 Mwt/ 3 shell</u>
Dresden 2	1600 Mwt	4.4 ft ³ /min	9.4
TVA Fossil Plants	700 MWe (average of 6)	6.7 ft ³ /min/shell	28.7
Quad Cities 1	2511 Mwt	9.6 ft ³ /min	13
Quad Cities 2	2511 Mwt	25 ft ³ /min	<u>34</u>
AVERAGE			21 cfm

2.2.9 HOLDUP TIMES FOR CHARCOAL DELAY SYSTEMS

2.2.9.1 Parameter

$T = 43.1 \text{ MK/P}$

where

K is the dynamic adsorption coefficient, in cm³/gm (see chart below);

M is the mass of charcoal adsorber, in 10³ lbs;

T is the holdup time, in hours; and

P is the thermal power level (Mwt) entered in Card 2

Dynamic adsorption coefficients (in cm³/gm) are as follows:

	<u>OPERATING 77°F DEW POINT 45°F</u>	<u>OPERATING 77°F DEW POINT -40°F</u>	<u>OPERATING 77°F DEW POINT 0°F</u>	<u>OPERATING 0°F DEW POINT -20°F</u>
Kr	18.5	70	25	105
Xe	330	1160	440	2410

2.2.9.2 Bases

Charcoal delay systems are evaluated using the above equation and dynamic adsorption coefficients. $T = \text{MK}/\text{flow rate}$ is a standard equation for the calculation of delay times in charcoal adsorption systems (Ref. 25). The dynamic adsorption coefficients (K values) for Xe and Kr are dependent on operating temperature and moisture content (Ref. 26 and 27) in the charcoal, as indicated by the values in the above parameter. The K values represent a composite of data from operating reactor charcoal delay systems (Refs. 28 and 30) and reports concerning charcoal adsorption systems (Refs. 26-28, 31-33).

The factors influencing the selection of K values are

- Operational data from KRB ($K_{Xe} = 20-30$, $K_{Kr} = 260-430$) (Ref. 28) and from KWL ($K_{Kr} = 30$, $K_{Xe} = 500$) (Ref. 29), and from Vermont Yankee (Ref. 31).
- The effect of temperature on the dynamic adsorption coefficients, indicated in Figure 2-2 (Ref. 26).
- The effect of moisture on the dynamic adsorption coefficients, shown in Figure 2-3. The affinity of charcoal for moisture, shown in Figure 2-4.
- The variation in K values between researchers and between the types of charcoal used in these systems (Refs. 26, 34, and 35). Because of the variation in K values based on different types of charcoal and the data reported, average values taken from KRB and KWL data shown in Figure 2-2 are used.

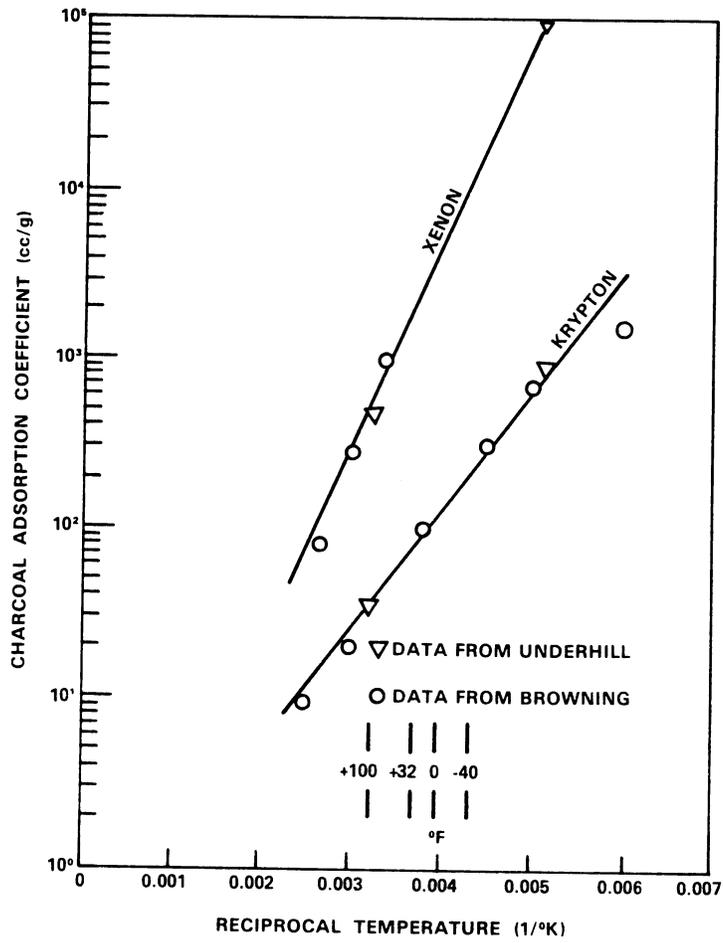


FIGURE 2-2
 KRYPTON AND XENON K VALUES AS A FUNCTION
 OF RECIPROCAL TEMPERATURE

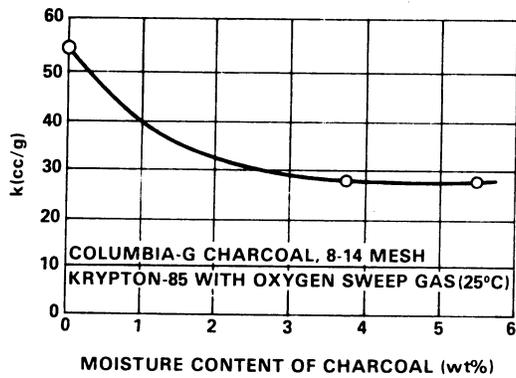


FIGURE 2-3
EFFECT OF MOISTURE CONTENT ON THE
DYNAMIC ADSORPTION COEFFICIENT

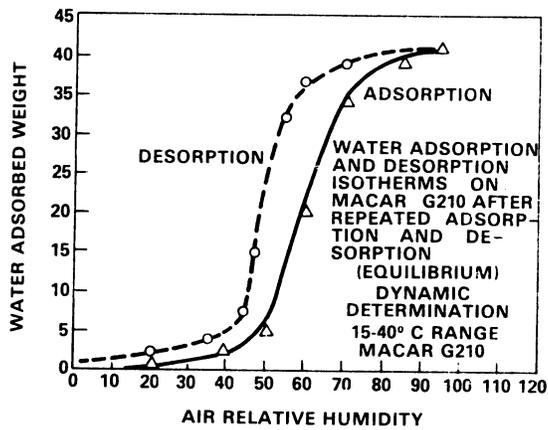


FIGURE 2-4
CHARCOAL MOISTURE AS A FUNCTION
OF RELATIVE HUMIDITY

The coefficient 43.1 adjusts the units and was calculated as follows:

$$T(\text{hr}) = \frac{M(10^3 \text{ lbs}) K(\text{cm}^3/\text{gm})(454 \text{ gm/lb})(3.53 \times 10^{-5} \text{ ft}^3/\text{cm}^3)}{(0.0062 \text{ ft}^3/\text{min/MWt}) (60 \text{ min/hr})P (\text{MWt})}$$

$$T = 43.1 \frac{MK}{P}$$

2.2.10 DECONTAMINATION FACTORS FOR CRYOGENIC DISTILLATION

2.2.10.1 Parameter

<u>NUCLIDES</u>	<u>DECONTAMINATION FACTOR</u>
I, Xe	1×10^4
Kr	4×10^3

The holdup times are calculated on the basis of gas residence time in the system prior to release.

2.2.10.2 Bases

A DF of 10^4 for iodine and xenon and a DF of 4×10^3 for krypton are used for a cryogenic distillation system. The values are based on data submitted in Amendment 11 to the PSAR for the Hope Creek Nuclear Generating Station, Units 1 and 2 (Ref. 36), which were derived from a proprietary report (Ref. 37) of Air Products and Chemical, Inc. The PSAR states that a maximum of 0.025% Kr (DF = 4×10^3) and 0.01% Xe (DF = 10^4) will escape from the system. These decontamination factors are considered reasonable.

2.2.11 RADIOIODINE REMOVAL EFFICIENCIES FOR CHARCOAL ADSORBERS AND PARTICULATE REMOVAL EFFICIENCIES FOR HEPA FILTERS

2.2.11.1 Parameter

Use a removal efficiency of 99% for particulate removal by HEPA filtration. For charcoal adsorbers, removal efficiencies for all forms of radioiodine are as follows:

<u>ACTIVATED CARBON BED DEPTH^a</u>	<u>ASSIGNED ACTIVATED CARBON REMOVAL EFFICIENCIES FOR RADIOIODINE</u>
2 inches. Air filtration system designed to operate inside primary containment.	90%
2 inches. Air filtration system designed to operate outside the primary containment and relative humidity is controlled to 70%.	70%
4 inches. Air filtration system designed to operate outside the primary containment and relative humidity is controlled to 70%.	90%
6 inches. Air filtration system designed to operate outside the primary containment and relative humidity is controlled to 70%.	99%

^aMultiple beds, e.g., two 2-inch beds in series, should be treated as a single bed of aggregate depth.

2.2.11.2 Bases

The removal efficiencies assigned HEPA filters for particulate removal and charcoal adsorbers for radioiodine removal are based on the design, testing and maintenance criteria recommended in Regulatory Guide 1.140, "Design, Testing and Maintenance Criteria for Normal Ventilation Exhaust System Air Filtration and Adsorption Units of Light-Water-Cooled Nuclear Power Plants" (Ref. 2).

2.2.12 LIQUID WASTE INPUTS

2.2.12.1 Parameter

The flow rates listed in Table 2-27 are used as inputs to the liquid radwaste treatment system. Flows that cannot be standardized are added to those listed in Table 2-27 to fit an individual application. Disposition of liquid streams to the appropriate collection tanks is based on the applicant's intended method of processing.

2.2.12.2 Bases

The liquid waste inputs are based on the values proposed by the ANS 55.3 Working Group in American National Standard, "Boiling Water Reactor Liquid Radioactive Waste Processing System," ANSI N197-1976 (Ref. 38). Activity inputs are based on the reactor coolant concentrations given in Parameter 2.2.3. The values given are those that were judged to be representative for a typical BWR design.

2.2.13 CHEMICAL WASTES FROM REGENERATION OF CONDENSATE DEMINERALIZERS

2.2.13.1 Parameter

1. Liquid flows to demineralizer at main steam activity.
2. All nuclides removed from the reactor coolant by the demineralizers are removed from the resins during regeneration.
3. Use a regeneration cycle of 3.5 days times the number of demineralizers. (For systems using ultrasonic resin cleaning, use 8 days times the number of demineralizers.)

2.2.13.2 Bases

Operating data from Dresden 2 and 3 indicate that one condensate demineralizer regeneration occurs every 3.5 days (Ref. 39) when ultrasonic cleaning is not used.

All material exchanged or filtered out by the resins between regenerations is contained in the regenerant waste streams; therefore, each regeneration will have approximately the same effectiveness (i.e., each regeneration removes all material collected since the previous regeneration, leaving a constant quantity of material on the resins after regeneration). Regeneration cycles are normally controlled by particulate buildup on resin beds, resulting in high pressure drops across the bed. If ultrasonic resin cleaning is used to remove insolubles between regenerations, operating data from Dresden 2 and 3 indicates that one condensate demineralizer regeneration occurs every 7.1 days (Ref. 40 and 41), from Pilgrim 1 at 8.2 days (Ref. 42) and from Nine Mile Point 1 at 10 days (Ref. 41).

2.2.14 DETERGENT WASTE

2.2.14.1 Parameter

For plants with an onsite laundry, use the radionuclide distribution given in Table 2-28 for untreated detergent wastes. The quantities shown in Table 2-28 are added to the adjusted liquid source term. They are reduced for any treatment provided using the appropriate decontamination factors.

2.2.14.2 Bases

In the evaluation of liquid radwaste treatment systems, it is assumed that detergent wastes (laundry drains, personnel and equipment decontamination drains, and cask cleaning drains) will total approximately 1000 gal/day per reactor. The radionuclide distribution given in Table 2-28 is based on data given in Table 2-29.

TABLE 2-27

BWR LIQUID WASTES

SOURCE	EXPECTED DAILY AVERAGE INPUT FLOW RATE (in gal/day)		FRACTION OF THE PRIMARY COOLANT ACTIVITY (PCA)
	DEEP BED PLANT WITH ULTRASONIC RESIN CLEANER	DEEP BED PLANT WITHOUT ULTRASONIC RESIN CLEANER OR A FILTER/DEMINERALIZER PLANT	
<u>Equipment Drains</u>			
Drywell	3,400	3,400	1.00
Containment, auxiliary building, and fuel pool	3,700	3,700	0.1
Radwaste building	1,100	1,100	0.1
Turbine building	3,000	3,000	0.001
Ultrasonic resin cleaner	15,000	-	0.05
Resin rinse*	2,500	5,000	0.002
<u>Floor Drains</u>			
Drywell	700	700	0.001
Containment, auxiliary building, and fuel handling	2,000	2,000	0.001
Radwaste building	1,000	1,000	0.001
Turbine building	2,000	2,000	0.001
<u>Other Sources</u>			
Cleanup phase separator decant	640	640	0.002
Laundry drains	1,000	1,000	-
Lab drains	500	500	0.02
Regenerants*	1,700	3,400	**
Condensate demineralizer backwash.	-	8,100	2×10^{-6}
Chemical lab waste	100	100	0.02

* Deep-bed condensate demineralizers only.

** Calculated by BWR-GALE Code.

† Filter/demineralizer (Powdex) condensate demineralizers only.

TABLE 2-28

CALCULATED ANNUAL RELEASE OF RADIOACTIVE MATERIALS
IN UNTREATED DETERGENT WASTE FOR A BWR

<u>NUCLIDE</u>	<u>Ci/yr</u>
C-14	2.8(-4)
P-32	1.7(-4)
Cr-51	9.1(-3)
Mn-54	4.6(-3)
Fe-55	9.6(-3)
Fe-59	1.6(-4)
Co-57	1.3(-4)
Co-56	9.3(-3)
Co-60	1.6(-2)
Ni-63	2.5(-4)
Sr-89	1.1(-4)
Sr-90	5.8(-5)
Y-91	1.6(-4)
Zr-95	1.5(-3)
Nb-95	1.8(-3)
Mo-99	6(-5)
Ru-103	3.1(-4)
Ru-106	3(-4)
Ag-110m	6(-4)
Sb-124	6.5(-4)
I-131	2(-3)
Cs-134	1.1(-2)
Cs-136	5.6(-4)
Cs-137	1.6(-2)
Ba-140	9.1(-4)
Ce-141	2(-4)
Ce-144	3.5(-3)
TOTAL	0.09 Ci

TABLE 2-29
 RADIONUCLIDE DISTRIBUTION OF DETERGENT WASTE
 (MILLICURIES/MONTH)

NUCLIDE	Oyster ^a Creek (1971-1973)	Ginna ^b (1972-1973)	Zion ^c (1977)	Fort Calhoun ^d (1977)
C-14	1.2(-2)	NA ^e	2(-2)	4.2(-2)
P-32	1.5(-2)	NA	NA	NA
Cr-51	2.3(-1)	NA	1.3	NA
Mn-54	1.3	1.1(-1)	1.3(-1)	2.2(-2)
Fe-55	3.5(-1)	NA	1.9	1.6(-1)
Fe-59	2.9(-2)	NA	2.6(-1)	NA
Co-57	7.5(-3)	NA	1.7(-2)	NA
Co-58	3.5(-1)	4.1(-1)	2.3	1(-1)
Co-60	3.8	9(-1)	9.1(-1)	4(-2)
Ni-63	NA	NA	3.5(-1)	7.1(-2)
Sr-89	2.1(-2)	NA	7(-3)	1.4(-3)
Sr-90	2.5(-3)	NA	7.4(-3)	NA
Y-91	NA	NA	1.4(-2)	NA
Zr-95	8.3(-2)	1.4(-1)	1.4(-1)	NA
Nb-95	1.6(-2)	2(-1)	2.7(-1)	NA
Mo-99	NA	5(-3)	NA	NA
Ru-103	1.3(-2)	1.4(-2)	5.2(-2)	NA
Ru-106	NA	2.5(-1)	NA	NA)
Ag-110m	NA	5(-2)	NA	NA
Sb-124	6.1(-2)	NA	4.7(-2)	NA
I-131	4.3(-1)	6(-2)	1.7(-1)	1.6(-2)
Cs-134	1.7(-1)	1.4	1.4	1.0
Cs-136	NA	NA	4.7(-2)	NA
Cs-137	2.9(-1)	2.5	2.0	1.2
Ba-140	7.6(-2)	NA	NA	NA
Ce-141	3.3(-2)	1(-3)	NA	NA
Ce-144	7.3(-2)	5.3(-1)	NA	NA
TOTAL	7.4	6.6	11.3	2.7

^aU.S.E.P.A., EPA-520/5-76-003, "Radiological Surveillance Studies at the Oyster Creek BWR Nuclear Generating Station," June 1976.

^bWestinghouse Corporation WCAP-8253, "Source Term Data for Westinghouse Pressurized Water Reactors," May 1974.

^cEG&G Idaho, Inc. and Allied Chemical Corp., Idaho National Engineering Laboratory, "Draft Report, In-Plant-Measurements at Zion Station," 1976.

^dNUREG/CR-0140, "In-Plant Source Term Measurements at Ft. Calhoun Station, Unit 1," August 1978.

^eNA, Radionuclides were not analyzed.

2.2.15 TRITIUM RELEASES

2.2.15.1 Parameter

The total tritium release through liquid and gaseous pathways is 0.03 Ci/yr per Mwt. The quantity of tritium released through the liquid pathway is approximately 50% of the total quantity of tritium calculated to be available for release. The remainder of the tritium produced is assumed to be released as a gas from building ventilation exhaust systems. 50% of the tritium in gaseous effluents is released from the turbine building ventilation system and the remaining 50% of the tritium in gaseous effluents is released from the containment building ventilation system. For "zero liquid release" plants, assign all of the tritium calculated to be available for release to building ventilation exhaust systems.

2.2.15.2 Bases

Table 2-30 lists the measured liquid and gaseous tritium releases from BWRs for 1972 through 1977. Based on the total tritium release for each facility, the integrated thermal power produced during the year, and a plant capacity factor of 80%, the total annual release is approximately 0.03 Ci/Mwt through the combined liquid and gaseous pathways.

The tritium can be released either in liquid wastes or as a gas with ventilation effluents, the relative amounts being dependent on liquid recycle practices. Table 2-31 lists the percentage of total tritium which is released in liquid effluents (based on the data in Table 2-30). The weighted average* indicates that approximately 50% of the tritium available for release is released in liquid effluents.

Tritium in gaseous effluents is released largely through building ventilation exhaust systems. Based on measurements taken in 1974 and 1975 of tritium release rates in building ventilation systems at Monticello, Vermont Yankee, and Oyster Creek (Ref.15), Table 2-32 provides the distribution of tritium released from various sources within the plant. Based on data in Table 2-32, approximately 50% of the tritium in gaseous effluents is released through the turbine building ventilation systems. Assuming that miscellaneous sources (radwaste building ventilation, fuel pool area) are released via the reactor building vent, the remaining 50% of the tritium in gaseous effluents is released through the reactor building ventilation system. Although it is recognized that tritium should be released via the gaseous pathway from the fuel handling area, data is available only from operating reactors (Mark I containments) where the spent fuel pool area is inside containment. It is not possible with the present data base to identify what fraction of the tritium from the reactor building is associated with the spent fuel pool area. Accordingly, until sufficient data is available, tritium releases from the spent fuel pool area will be considered to be released from the containment building, even if the spent fuel pool is located elsewhere (BWR/6 Mark III's).

2.2.16 DECONTAMINATION FACTORS FOR DEMINERALIZERS

2.2.16.1 Parameter

The following are the expected decontamination factor (DFs) for demineralizers used on process or radwaste streams.

DEMINERALIZER TYPE	DECONTAMINATION FACTORS*		
	ANION	Cs, Rb	OTHER NUCLIDES
<u>Mixed Bed (H⁺ OH⁻)</u>			
Reactor Coolant	10	2	10
Condensate	10	2	10
Clean waste	10 ² (10)	10(10)	10 ² (10)
Dirty waste (floor drains)	10 ² (10)	2(10)	10 ² (10)
<u>Cation Bed (H⁺)</u>			
Dirty waste	1(1)	10(10)	10 ² (10)
<u>Powdex (any system)</u>	10(10)	2(10)	10(10)

*For an evaporator polishing demineralizer or for the second demineralizer in series, the DF is given in the parentheses.

TABLE 2-30

TRITIUM RELEASE DATA FROM OPERATING BWRs*

REACTOR NAME	POWER STARTUP MWT DATE	NUCLEAR THERMAL OUTPUT 10 ⁶ MWDt							TRITIUM RELEASED (Ci/yr)							TOTAL TRITIUM RELEASED (Ci/yr-Mwt at 80% capacity)															
									GASEOUS			LIQUID																			
		1972	1973	1974	1975	1976	1977	1978	1972	1973	1974	1975	1976	1977	1978	1972	1973	1974	1975	1976	1977	1978	1972	1973	1974	1975	1976	1977	1978		
Oyster Creek	1930 1969	0.54	0.45	0.46	0.41	0.49	0.41	0.8	0.4	0.4	2.8	1.1	0.7	62	36.6	14.1	18	38	3.4	0.034	0.024	0.009	0.015	0.023	0.003	0.034	0.024	0.009	0.015	0.023	0.003
Nine Mile Point 1	1850 1969	0.42	0.46	0.44	0.40	0.55	0.38	18	26.8	**	20	19	33	28	46.5	18.7	28	2.5	0.5	0.032	0.047	0.012	0.035	0.011	0.026	0.032	0.047	0.012	0.035	0.011	0.026
Dresden 2/3	2577 1970/71	1.04	1.18	0.91	0.70	1.15	1.20	31	10	11	220	170	330	26	26	22.6	54	20	0.1	0.016	0.009	0.011	0.11	0.048	0.081	0.016	0.009	0.011	0.11	0.048	0.081
Millstone 1	2011 1970	0.40	0.25	0.47	0.50	0.48	0.62	4.2	1.7	2.8	17	29	33	21	3.7	24.1	80	20	7.5	0.018	0.006	0.017	0.057	0.030	0.019	0.018	0.006	0.017	0.057	0.030	0.019
Monticello	1670 1970	0.46	0.41	0.37	0.37	0.51	0.46	12	**	**	66	77	139	***	***	***	0	0	0	0.008	-	-	0.052	0.044	0.088	0.008	-	-	0.052	0.044	0.088
Vermont Yankee	1593 1972	0.06	0.18	0.34	0.47	0.42	0.46	+	1.0	0.9	7.1	14	28	+	0.2	***	0	1.6	0.1	-	0.002	0.001	0.004	0.011	0.018	-	0.002	0.001	0.004	0.011	0.018
Quad Cities 1/2	2511 1971/72	0.52	1.32	1.09	0.96	1.08	1.12	4.7	34++	29	280	300	40	4.7	24.5	34	54	24	19	0.005	0.013	0.017	0.10	0.088	0.016	0.005	0.013	0.017	0.10	0.088	0.016
Pilgrim 1	1998 1972	0.11	0.53	0.25	0.34	0.32	0.34	**	14	8	74	37	61	4.2	0.4	10.4	18	47	33	0.011	0.008	0.22	0.079	0.077	0.080	0.011	0.008	0.22	0.079	0.077	0.080
Peach Bottom 2/3	3293 1973/74																														
Browns Ferry 1-3	3293 73/74/76																														
Cooper	2381 1974																														
Hatch 1	2436 1974																														
Fitzpatrick	2436 1974																														
Duane Arnold	1658 1974																														
Brunswick 1/2	2436 1975/76																														
WEIGHTED AVERAGE+++																															

* Data from semiannual reports of reactor listed.

** No reported data.

*** No measurement made.

† Prior to first refueling.

++ Measured only during the July-December 1973 period.

+++ Average weighted by nuclear thermal output.

Data for first half of 1977 have been extrapolated to the end of 1977 for Oyster Creek, Nine Mile Point-1, Millstone-1, Monticello, Browns Ferry 1, 2 and 3, Hatch-1, Fitzpatrick and Brunswick 1 and 2.

TABLE 2-31

TRITIUM RELEASE DATA FROM OPERATING BWR'S
PERCENT OF TOTAL TRITIUM RELEASED IN LIQUID EFFLUENTS

<u>REACTOR</u>	<u>1972</u>	<u>1973</u>	<u>1974</u>	<u>1975</u>	<u>1976</u>	<u>1977</u>
Oyster Creek	98.7	91.5	97.2	86.5	97.2	69.4
Nine Mile Point 1	60.9	63.4	**	58.3	11.6	1.6
Dresden 2/3	45.6	72.2	67.3	31.0	10.5	0
Millstone 1	83.3	68.5	89.6	82.5	40.8	18.6
Monticello	**	**	**	0	0	0
Vermont Yankee		16.7	**	0	10.3	0.4
Quad Cities 1/2	50.0	41.9	54.0	16.2	7.4	32.5
Pilgrim 1	**	2.8	56.8	19.6	56.0	35.1
Peach Bottom 2/3				99.0	73.3	21.5
Browns Ferry 1/2/3				66.2	87.3	47.7
Cooper				16.2	11.0	15.3
Hatch 1				77.2	86.5	92.1
Fitzpatrick				**	21.9	22.5
Duane Arnold				1.5	2.0	1.4
Brunswick 1/2				61.5	21.1	27.8
*Weighted Average	63.4	53.1	69.5	51.4	36.2	28.2

*Average weighted by thermal nuclear output

**Insufficient Data

*Prior to first refueling

TABLE 2-32

DISTRIBUTION OF TRITIUM RELEASE IN GASEOUS EFFLUENTS (Ref. 15)

PLANT	SOURCE OF GASEOUS TRITIUM RELEASE (% OF TOTAL)			TOTAL
	REACTOR BUILDING	TURBINE BUILDING	MISCELLANEOUS	
Monticello	68	29	3	100
Vermont Yankee	35	53	12	100
Oyster Creek	13	79	8	100
AVERAGE	39	54	7	100

2.2.16.2 Bases

The DFs for demineralizers used in the evaluation of liquid waste treatment systems are derived from the findings of a generic review in the nuclear industry by ORNL (Ref. 41). This reference contains operating and theoretical data that provides a basis for the numerical values assigned. The information contained in this report was projected to obtain a performance value expected over an extended period of operation. It was also considered that attempts to extend the service life of the resin will reduce the DFs below those expected under controlled operating conditions.

The following operating conditions were factored into the evaluation of demineralizer performance:

1. In general, the DF for waste treatment systems will vary with the quality of the water to be treated, increasing with increasing activity. Normally, when two demineralizers are used in series, the first demineralizer will have a higher DF than the second. However, the data in Reference 41 indicate that Cs and Rb will be more strongly exchanged in the second demineralizer in series than in the first, since the concentration of preferentially exchanged competing nuclides is reduced.

2. As indicated in Reference 41, compounds of Y, Mo, and Tc form colloidal particles that tend to plate out on solid surfaces. Mechanisms such as plateout on the relatively large surface area provided by demineralizer resin lead to removal of these nuclides to the degree stated above. An analysis of effluent release data indicates that these nuclides, although present in the primary coolant, are normally undetectable in the effluent streams.

2.2.17 DECONTAMINATION FACTORS FOR EVAPORATORS

2.2.17.1 Parameter

	<u>ALL NUCLIDES EXCEPT ANIONS</u>	<u>ANIONS</u>
Miscellaneous radwaste evaporator	10^4	10^3
Separate evaporator for detergent wastes	10^2	10^2

2.2.17.2 Bases

The decontamination factors for evaporators are derived from the findings of a generic review by ORNL of evaporators used in the nuclear industry (Ref. 43). The principal conclusions reached in the report are:

1. Decontamination factors of 10^4 can be expected for nonvolatile radioactive nuclides in a single-stage evaporator.
2. Decontamination factors for iodine are a factor of 10 less than the DFs for nonvolatile nuclides (10^3).
3. Decontamination factors for wastes containing detergents that tend to foam are a factor of 10 to 100 lower than DFs expected for nonfoaming wastes.

These conclusions have been extended to take into account the following factors:

1. For nonvolatile nuclides in a nonfoaming solution, a DF of 10^4 is used.
2. For iodine in a nonfoaming solution, a DF of 10^3 is used.
3. If an evaporator is used for detergent wastes, the DF for the evaporator is reduced to 100 to reflect carryover due to foaming, which will reduce the DF.

2.2.18 DECONTAMINATION FACTORS FOR REVERSE OSMOSIS

2.2.18.1 Parameter

Overall DF of 30 for laundry wastes and DF of 10 for other liquid radwastes.

2.2.18.2 Bases

Reverse osmosis processes are generally run as semibatch processes. The concentrated stream rejected by the membrane is recycled until a desired fraction of the batch is processed through the membrane. The ratio of the volume processed through the membrane to the inlet batch volume is the percent recovery. The DF normally specified for the process is the ratio of nuclide concentrations in the concentrated liquor stream to the concentrations in the effluent stream. This ratio is termed as the membrane DF. For source term calculations, the system DF should be used. The system DF is the ratio of the nuclide concentrations in the feed stream to those in the effluent stream. The relationship between the system DF and the membrane DF is nonlinear and is a function of the percent recovery. This relationship can be expressed as follows:

$$DF_s = \frac{F}{1 - [1 - F]^{1/DF_m}}$$

where

DF_m is the membrane DF;

DF_s is the system DF; and

F is the ratio of effluent volume to inlet volume (percent recovery).

Tables 2-33 through 2-35 give membrane DFs derived from operating data at Point Beach and Ginna (Refs. 45 and 46) and laboratory data on simulated radwaste liquids (Ref. 47). These data indicate that the overall membrane DF is approximately 100. The percent recovery for liquid radwaste processes using reverse osmosis is expected to be approximately 95%, i.e., 5% concentrated liquor. Using these values in the above equation, the system DF is approximately 30.

$$DF_s = \frac{0.95}{1 - (1 - .95)^{1/100}} = 30$$

The data used were derived mainly from tests on laundry wastes. The DF for other plant wastes, e.g., floor drain wastes, is expected to be lower because of the higher concentrations of iodine and cesium isotopes. As indicated by the data in Tables 2-33 and 2-35, the membrane DF for these isotopes is lower than the average membrane DF used in the evaluation for laundry waste.

2.2.19 DECONTAMINATION FACTORS FOR LIQUID RADWASTE FILTERS

2.2.19.1 Parameter

A DF of 1 for liquid radwaste filters is assigned for all radionuclides.

2.2.19.2 Bases

Reference 44 contains the findings of a generic review by ORNL of liquid radwaste filters used in the nuclear industry. Due to the various filter types and filter media employed, reported decontamination factors vary widely, with no discernible trend. The principal conclusion reached in the ORNL report is that no credit should be assigned liquid radwaste filters (DF of 1) until a larger data base is obtained.

2.2.20 ADJUSTMENT TO LIQUID RADWASTE SOURCE TERMS FOR ANTICIPATED OPERATIONAL OCCURRENCES

2.2.20.1 Parameter

1. Increase the calculated source term by 0.1 Ci/yr per reactor using the same isotopic distribution as for the calculated source term to account for anticipated operational occurrences such as operator errors that result in unplanned releases.

2. Assume evaporators to be unavailable for two consecutive days per week for maintenance. If a 2-day holdup capacity exists in the system (including surge tanks) or an alternative evaporator is available, no adjustment is needed. If less than a 2-day capacity is available, assume the waste excess is handled as follows:

TABLE 2-33

REVERSE OSMOSIS DECONTAMINATION FACTORS, GINNA STATION

<u>NUCLIDE</u>	<u>FEED ACTIVITY</u> <u>($\mu\text{Ci}/\text{cm}^3$)</u>	<u>PRODUCT ACTIVITY</u> <u>($\mu\text{Ci}/\text{cm}^3$)</u>	<u>MEMBRANE DF</u>
Ce-144	2.68×10^{-4}	$<2.2 \times 10^{-7}$	1200
Co-58	8.55×10^{-5}	$<3.4 \times 10^{-8}$	2500
Ru-103	5.83×10^{-5}	$<5.5 \times 10^{-8}$	1100
Cs-137	4.09×10^{-4}	6.6×10^{-6}	60
Cs-134	2.02×10^{-4}	3.2×10^{-6}	60
Nb-95	5.35×10^{-5}	$<5.3 \times 10^{-8}$	1000
Zr-95	2.36×10^{-5}	$<3.7 \times 10^{-8}$	640
Mn-54	8.82×10^{-5}	$<3.4 \times 10^{-8}$	2600
Co-60	9.62×10^{-4}	$<8.1 \times 10^{-8}$	12,000
Total isotopic	2.15×10^{-3}	9.8×10^{-6}	220
Gross β	1.63×10^{-3}	1.86×10^{-5}	88
Average*			200

*The average DF is calculated from the average of the reciprocals of the isotopic DFs.

TABLE 2-34
 REVERSE OSMOSIS DECONTAMINATION FACTORS, POINT BEACH

<u>DATE</u>	<u>TIME</u>	<u>FEED ACTIVITY</u> ($\mu\text{Ci}/\text{ml}$)	<u>PRODUCT ACTIVITY</u> ($\mu\text{Ci}/\text{ml}$)	<u>MEMBRANE</u> <u>DF</u>
6/14/71	0840	1.1×10^{-5}	6.8×10^{-7}	16
	1225	6.3×10^{-5}	4.2×10^{-7}	150
	1530	8.8×10^{-5}	3.2×10^{-7}	280
6/15/71	1030	2.7×10^{-4}	3.1×10^{-6}	87
	1315	1.0×10^{-4}	1.7×10^{-6}	59
	1440	1.3×10^{-4}	1.1×10^{-7}	1200
	1510	1.6×10^{-4}	1.1×10^{-7}	1500
	1530	1.8×10^{-4}	5.7×10^{-7}	320

TABLE 2-35
 EXPECTED REVERSE OSMOSIS DECONTAMINATION FACTORS
 FOR SPECIFIC NUCLIDES

<u>NUCLIDE</u>	<u>FEED ACTIVITY</u> ($\mu\text{Ci}/\text{ml}$)	<u>PRODUCT ACTIVITY</u> ($\mu\text{Ci}/\text{ml}$)	<u>MEMBRANE</u> <u>DF</u>
Co-60	2.5×10^{-4}	5×10^{-7}	500
Mo-99	3.8×10^{-2}	1×10^{-3}	40
I-131, 132, 133, 134, 135	1.2×10^{-1}	4×10^{-3}	30
Cs-134, 137	4.3×10^{-2}	2×10^{-4}	200

a. High-purity or low-purity waste Processed through an alternative system (if available) using a discharge fraction consistent with the lower purity system.

b. Chemical Waste Discharged to the environment to the extent holdup capacity or an alternative evaporator is unavailable.

3. The following methods should be used for calculating holdup times and effective system DF:

a. Holdup Capacity If two or more holdup tanks are available, assume one tank is full (80% capacity) with the remaining tanks empty at the start of the two day outage. If there is only one holdup tank, assume that it is 40% full at the start of the two day outage with a usable capacity of 80%.

b. Effective System DF Should the reserve storage capacity be inadequate for waste holdup over a two-day evaporator outage, and should an alternate evaporator be unavailable to process the wastes from the out-of-service evaporator, the subsystem DF should be adjusted to show the effect of the evaporator outage.

For example, a DF of 10^5 was calculated for a radwaste demineralizer and radwaste evaporator in series. If an adjustment were required for the evaporator being out-of-service two days/week, with only one day holdup tank capacity, then the effective system DF can be calculated as follows:

1. For 6 days (7 - 2 + 1) out of 7 the system DF would be 10^5 .
2. For the remaining one day, the system DF would be 10^2 (only the demineralizer DF is considered). The effective DF is:

$$DF = \left[\left(\frac{6}{7} \right) (10^{-5}) + \left(\frac{1}{7} \right) (10^{-2}) \right]^{-1} = 7.0 \times 10^2$$

2.2.20.2 Bases

Reactor operating data over an 8 year period, January 1970 through December 1977, representing 127 reactor years of operation were evaluated to determine the frequency and extent of unplanned liquid releases. During the period evaluated, 50 unplanned liquid releases occurred; 28 due to operator errors, 13 due to component failures, 5 due to inadequate procedures or failure to follow procedures, and the remainder (4) due to miscellaneous causes such as design errors. Table 2-36 summarizes the findings of this evaluation. Based on the data provided in Table 2-36 it is estimated that 0.1 Ci/yr/reactor will be discharged in unplanned releases in liquid effluents. Tritium releases for BWR anticipated operational occurrences were less than 1% of the total normal operational release value, and was, therefore, judged to be negligible.

The availability for evaporators in waste treatment systems is expected to be in the range of 60 to 80%. Unavailability is attributed to scaling, fouling of surfaces, instrumentation failures, corrosion, and occasional upsets resulting in high carryovers requiring system cleaning. A value of two consecutive days unavailability per week was chosen as being representative of operating experience. For systems having sufficient tank capacity to collect and hold wastes during the assumed 2-day/week outage, no adjustments are required for the source term. If less capacity is available, the difference between the waste expected during two days of normal operation and the available holdup capacity is assumed to follow an alternative route for processing. Since processing through an alternative route implies mixing of wastes having different purities and different dispositions after treatment, it is assumed that the fraction of waste discharged following processing will be that normally assumed for the less pure of the two waste streams combined.

Since chemical and regenerant wastes are not amenable to processes other than evaporation, it is assumed that unless an alternative evaporation route is available, chemical and regenerant wastes in excess of the storage capacity are discharged without treatment.

2.2.21 GUIDELINES FOR ROUNDING OFF NUMERICAL VALUES

In calculating the estimated annual release of radioactive materials in liquid and gaseous wastes, round off all numerical values to two significant figures.

TABLE 2-36

FREQUENCY AND EXTENT OF UNPLANNED LIQUID RADWASTE
RELEASES FROM OPERATING PLANTS*

<u>UNPLANNED LIQUID RELEASES</u>	
Total number (unplanned releases)	50
Fraction due to personnel error	0.56
Fraction due to component failure	0.26
Fraction due to inadequate procedures or failure to follow procedures	0.10
Fraction due to other causes	0.08
Approximate activity (Ci)	10.62
Fraction of cumulative occurrences per reactor year (plants reporting releases >5 gals of liquid waste/reactor year)	0.15
Fraction of cumulative occurrences per reactor year (plants reporting activity released >0.01 mCi/reactor year)	0.27
Activity per release (Ci/release)	0.30
Activity released per reactor year (Ci/reactor/year)	0.10
Volume of release per reactor year (gal/reactor year)	1.66×10^4

*Values in this table are based on reported values in 1970-1977 Licensee Event Reports

2.2.22 CARBON-14 RELEASES

2.2.22.1 Parameter

The estimated annual quantity of carbon-14 released from a boiling water reactor is 9.5 Ci/yr. It is assumed that the carbon-14 reacts with oxygen in the reactor water and behaves like a noble gas fission product; thus all carbon-14 produced will be released through the main condenser offgas system.

2.2.22.2 Bases

The principal source of carbon-14 is the thermal neutron reaction with oxygen-17 in the reactor coolant. The production rate of carbon-14 from oxygen-17 is given by the equation:

$$Q = N_o \sigma_o \phi m t p s \quad (\text{Ci/yr})$$

where

- m is the 3.9×10^4 kg, mass of water in reactor core;
- N_o is the 1.3×10^{22} atoms O-17/kg natural water;
- p is the 0.80, plant capacity factor;
- s is the 1.03×10^{-22} Ci/atom, specific activity for C-14;
- t is the 3.15×10^7 sec/yr, maximum irradiation time per year;
- σ_o is the 2.4×10^{-25} cm², thermal neutron cross section for O-17; and
- ϕ is the 3×10^{13} neutrons/cm²-sec, average thermal neutron flux.

Based on the above parameters, $Q = 9.5$ Ci/yr.

Carbon-14 can also be produced by neutron activation of nitrogen-14 dissolved in the reactor coolant and present in air in the drywell. These sources contribute a small fraction of a curie per year to the annual production of carbon-14 due to the low concentration of nitrogen-14 in the reactor coolant (less than 1 ppm by weight), and the low neutron flux in the drywell (approximately 4×10^8 neutrons/cm²-sec).

The annual release of 9.5 Ci of carbon-14 is in good agreement with measurements at Nine Mile Point 1 reported by Kunz et al. (Ref. 48), who found that 8 curies per year of carbon-14 were released, principally in the form of CO₂.

2.2.23 ARGON-41 RELEASES

The argon-41 input to the main condenser offgas treatment system (MCOTS) downstream of the air ejectors, is 40 μ Ci/sec. The dynamic adsorption coefficients for argon-41 in charcoal delay beds of a MCOTS are 6.4 cm³/gm for an ambient temperature charcoal system and 16 cm³/gm for a chilled charcoal system. The holdup time for argon-41 in a charcoal delay system is determined using the equation in Section 2.2.9.1.

The argon-41 release from the purging or venting of the drywell is 15 Ci/yr.

2.2.23.2 Bases

Argon-41 is formed by neutron activation of stable naturally occurring argon-40. This reaction may occur with argon-40 present in the reactor coolant and also with argon-40 in the drywell air surrounding the reactor vessel.

Argon-40 will enter the reactor coolant as a part of air inleakage at or downstream of the main condenser. Argon-41 produced by activation of the argon-40 in the reactor vessel will be transported to the main condenser offgas treatment system (MCOTS). Data in reference 49 and summarized in Table 2-37 indicates that the argon-41 input to the MCOTS during the measurements ranged from 5.6 μ Ci/sec to 37 μ Ci/sec. Due to the limited duration of these measurements, the mean value of the data is not used. Instead, in these evaluations a release rate of 40 μ Ci/sec is considered to be a value that is not likely to be exceeded, on the average, over the 30 year life of the plant.

Argon-41 will be held up in charcoal delay beds of the MCOTS in the same manner as discussed for xenon and krypton in Section 2.2.9.2. Values of the dynamic adsorption

coefficient are based on data contained in references 49, 50 and 51 for ambient and chilled temperature systems. Holdup times for argon-41 are determined using these k values and the delay equation in Section 2.2.9.1.

Argon-41 release from the drywell are based on data in reference 49 concerning the neutron flux in the drywell and on an assumed drywell purging frequency of 24 purges per year.

TABLE 2-37
 SUMMARY OF ARGON-41 RELEASES
 TO THE MAIN CONDENSER OFFGAS TREATMENT SYSTEM*
 ($\mu\text{Ci}/\text{sec}$)

<u>PLANT</u>	<u>Argon-41 Release</u>
Browns Ferry 1	38
Browns Ferry 2	17
"	12
Browns Ferry 3	7.1
"	5.8
"	7.4
"	34
"	32
"	19
Hatch 1	12
"	16
Fitzpatrick	36

* Data in this table are based on measured argon-41 release rates in reference 49 and were adjusted to 3400 Mwt.

CHAPTER 3. INPUT FORMAT, SAMPLE PROBLEM, AND
FORTRAN LISTING OF THE BWR-GALE CODE

3.1 INTRODUCTION

This chapter contains additional information for using the BWR-GALE Code. Chapter 1 of this report described the entries required to be entered on input data cards, and Section 3.2 of this chapter contains sample input data sheets and flow charts to orient the user in making the entries described in Chapter 1.

Section 3.3 of this chapter contains a listing of the input data cards for a sample problem and the resultant output for that sample problem. Section 3.4 contains a discussion of the nuclear data library used and a FORTRAN listing of the BWR-GALE Code.

3.2 INPUT DATA SHEETS

The following pages (3-3 through 3-11) show (1) the form in which data should be entered on input data sheets and (2) a sample completed sheet and flow sheets for both the liquid and gas codes.

3.3 SAMPLE PROBLEM - INPUT AND OUTPUT

The following pages (3-12 through 3-18) show printouts of the input and output for a sample problem using the BWR-GALE Code.

3.4 LISTING OF BWR-GALE CODE

3.4.1 NUCLEAR DATA LIBRARY

Calculation of the releases of radioactive materials in liquid effluents using the GALE Code requires a library of nuclear data available from the Division of ADP Support, USNRC (301)492-7713. For convenience, the tape consists of five files, written in card image form. The contents of the five files are:

1. File 1: A FORTRAN listing of the liquid effluent code.
2. File 2: Nuclear data library for corrosion and activation products for use with the liquid effluent code.
3. File 3: Nuclear data library for fuel materials and their transmutation products for use with the liquid effluent code.
4. File 4: Nuclear data library for fission products for use with the liquid effluent code.
5. File 5: A FORTRAN listing of the gaseous effluent code.

The tape is written in the following format:

DCB = (RECFM = FB, LRECL = 80, BLKSIZE = 3200)

Use of the tape requires two data cards in addition to those described in Chapter 1 containing the plant parameters. For a low enrichment uranium-235 oxide-fueled light water reactor, these cards should always contain the following data:

<u>CARD</u>	<u>COLUMN</u>	<u>INPUT DATA</u>
1	1-72	Title
1	75	The value 2
2	1-10	The value 0.632
2	11-20	The value 0.333
2	21-30	The value 2.0
2	31-40	The value 1.0E-25
2	41-46	The date (month, day, year)
2	48	The value 1
2	50	The value 0
2	52	The value 0

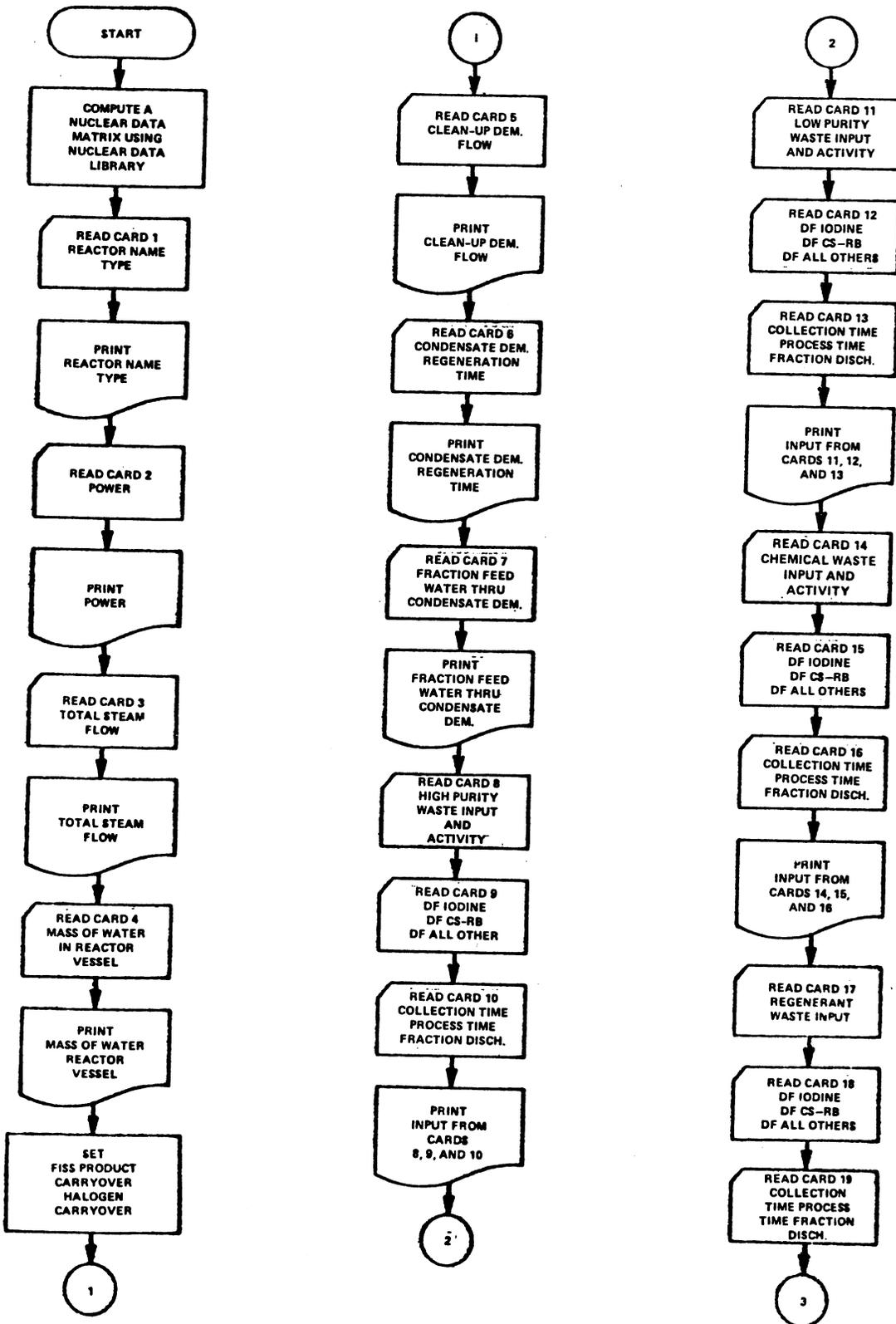
A description of the information contained in the nuclear data library can be found in the report ORNL-4628, "ORIGEN - The ORNL Isotope Generation and Depletion Code," dated May 1973.

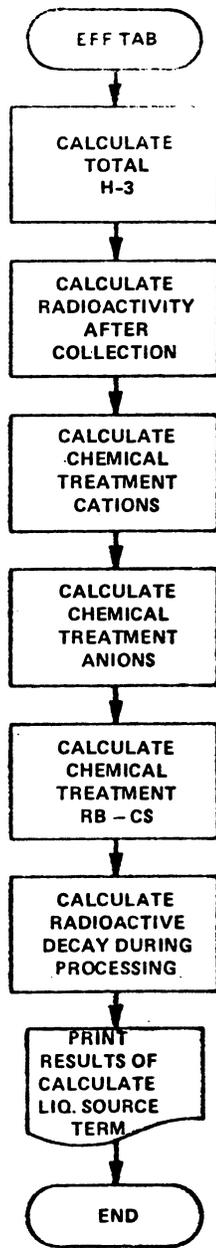
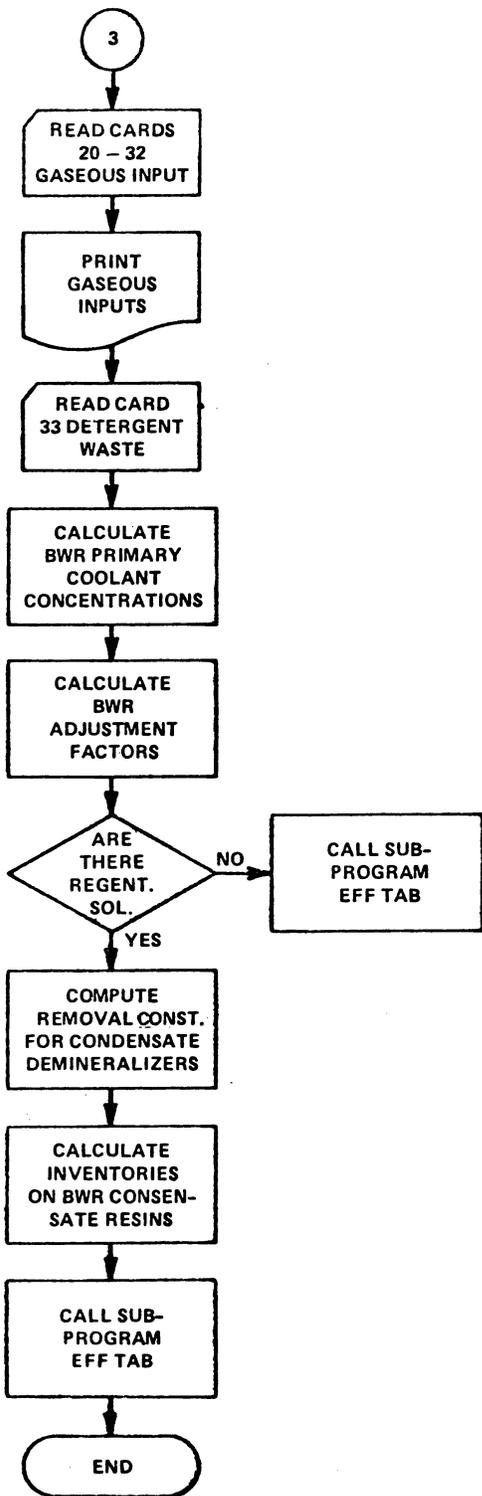
3.4.2 FORTRAN PROGRAM LISTING

The remainder of this chapter (pages 3-19 through 3-58) provides the program listing for the BWR-GALE Code.

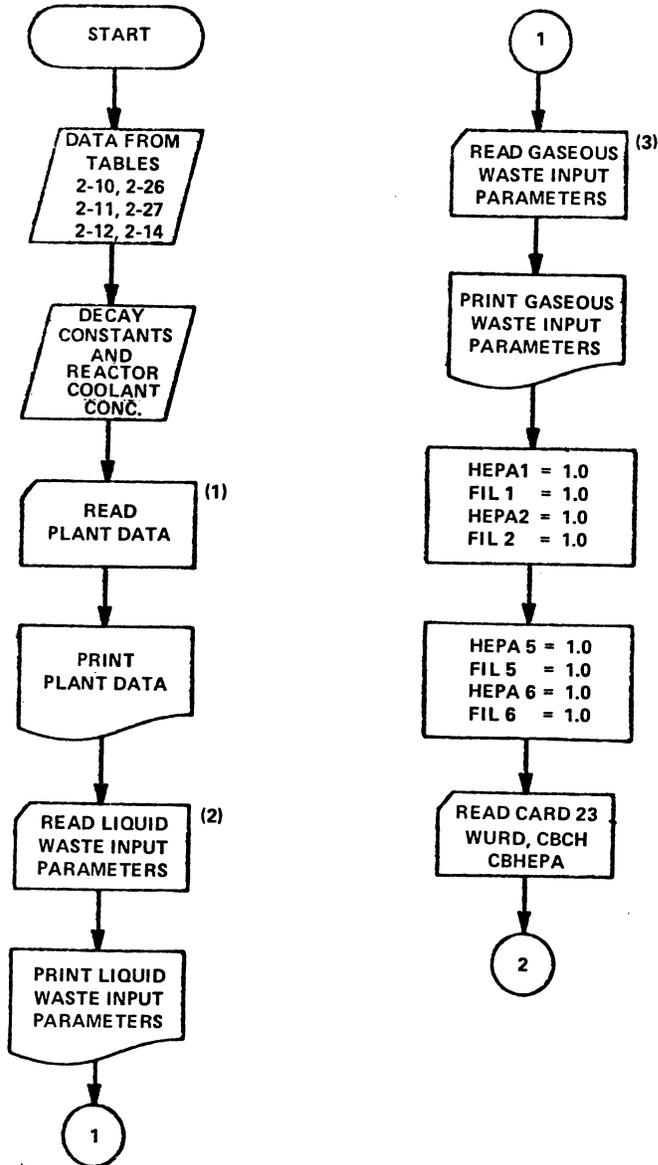
CARD	NAME	NAME OF REACTOR	SAMPLE BWR CASE 1	TYPE =	BWR
CARD 1	POWTH	THERMAL POWER LEVEL (MEGAWATTS)			3400.
CARD 2	GTO	TOTAL STEAM FLOW (MILLION LBS/HR)			15.
CARD 3	WL1Q	MASS OF WATER IN REACTOR VESSEL (MILLION LBS)			0.38
CARD 4	GDE	CLEAN-UP DEMINERALIZER FLOW (MILLION LBS/HR)			0.13
CARD 5	REGENT	CONDENSATE DEMINERALIZER REGENERATION TIME (DAYS)			56.
CARD 6	FFCDM	FRACTION FEED WATER THROUGH CONDENSATE DEMIN			1.00
CARD 7		HIGH PURITY WASTE INPUT 28640. GPD AT .15 PCA			
CARD 8		DFI= 1.0E03DFCS= 1.0E02DFO = 1.0E03			
CARD 9		COLLECTION 1.0 DAYS PROCESS 0.07 DAYS FRACT DISCH			0.01
CARD 10		LOW PURITY WASTE INPUT 5700. GPD AT .13			
CARD 11		DFI= 1.0E03DFCS= 1.0E04DFO = 1.0E04			
CARD 12		COLLECTION 3.10 DAYS PROCESS 0.6 DAYS FRACT DISCH			1.0
CARD 13		CHEMICAL WASTE INPUT 600. GPD AT .02 PCA			
CARD 14		DFI= 1.0E03DFCS= 1.0E04DFO = 1.0E04			
CARD 15		COLLECTION 3.1 DAYS PROCESS .60 DAYS FRACT DISCH			1.0
CARD 16		REGENERATION SOLTNS INPUT GPD			1700.
CARD 17		DFI= 1.0E04DFCS= 1.0E05DFO = 1.0E05			
CARD 18		COLLECTION 9.4 DAYS PROCESS .44 DAYS FRACT DISCH			1.0
CARD 19	GGS	GLAND SEAL STEAM FLOW (THOUSAND LBS/HR)			0.0
CARD 20	TIM3	GLAND SEAL HOLDUP TIME (HOURS)			0.0
CARD 21	TIM4	AIR EJECTOR OFFGAS HOLDUP TIME (HOURS)			.167
CARD 22		CONTAINMENT BLDG. CHARCOAL 90.0 HEPA?99.0			
CARD 23		TURBINE BLDG. CHARCOAL 00.0 HEPA?00.0			
CARD 24	FIL3	GLAND SEAL VENT, IODINE PF			00.0
CARD 25	FIL4	AIR EJECTOR OFFGAS IODINE PF			1.0
CARD 26		AUXILIARY BLDG. CHARCOAL 00.0 HEPA?00.0			
CARD 27		RADWASTE BLDG. CHARCOAL 00.0 HEPA?99.0			
CARD 28	KCHAR	CHARCOAL DELAY SYSTEM 0=NO,1=YES,2=CRYOGENIC DISTILL			105.0
CARD 29	KKR	KRYPTON DYNAMIC ADSORPTION COEFFICIENT (CM3/GM)			2410.0
CARD 30	KXE	XENON DYNAMIC ADSORPTION COEFFICIENT (CM3/GM)			48.
CARD 31	KMASS	MASS OF CHARCOAL (THOUSAND LBS)			1.0
CARD 32	PFLAUN	DETERGENT WASTE DECONTAMINATION FACTOR			
CARD 33					

FLOW CHART FOR BWR LIQUID CODE

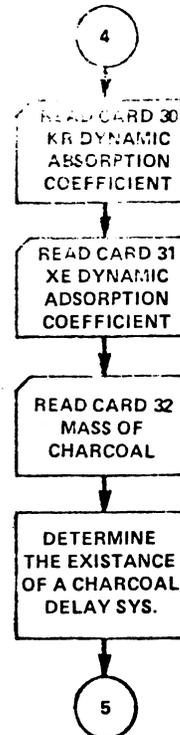
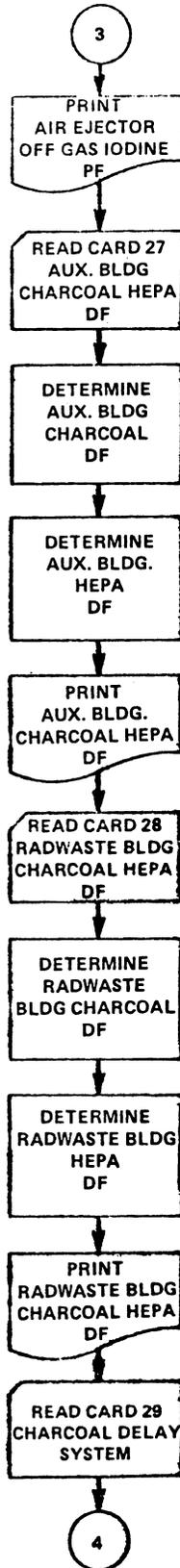
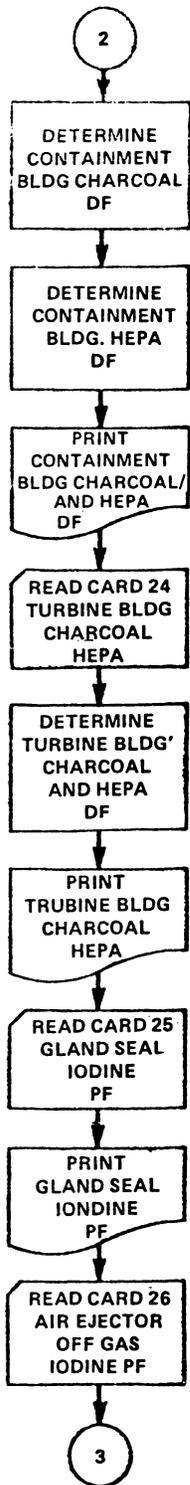




FLOWCHART FOR BWR GAS CODE



- (1) SEE SAMPLE INPUT CARDS 1 THRU 7.
 (2) SEE SAMPLE INPUT CARDS 8 THRU 19.
 (3) SEE SAMPLE INPUT CARDS 20 THRU 22.



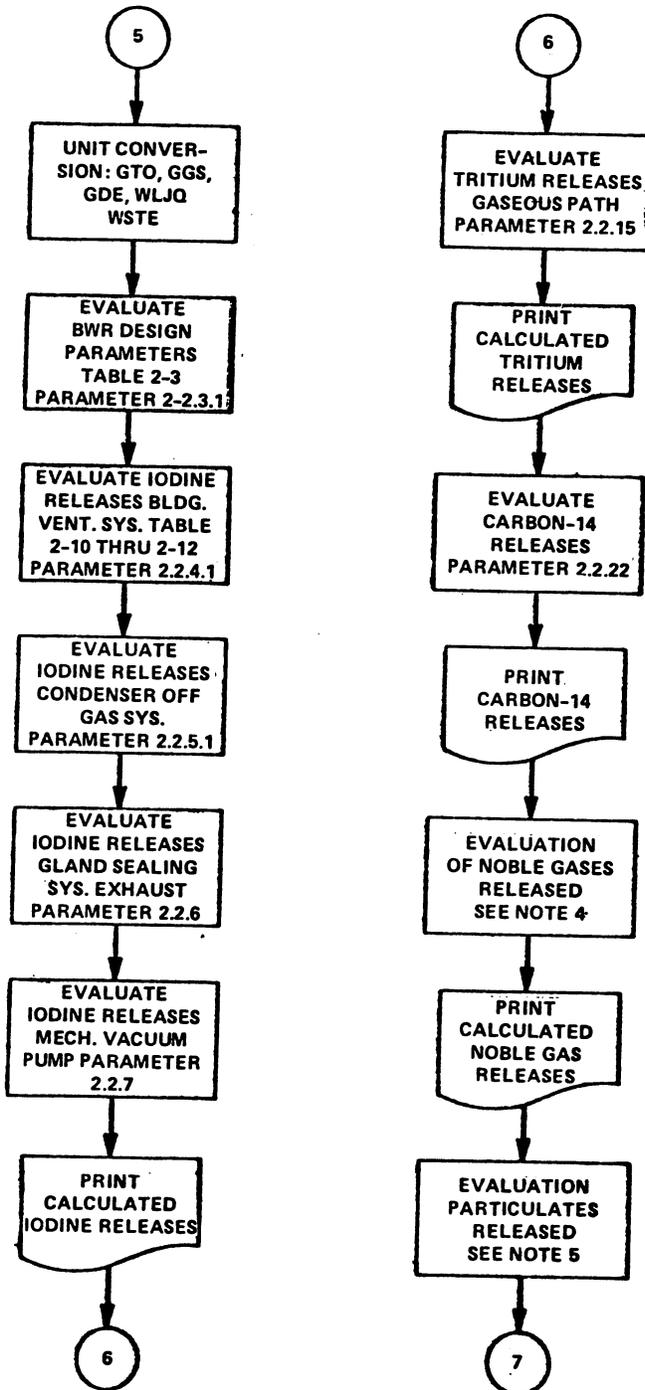


TABLE 2-14. PARAMETERS 2.2.9, 2.2.7, 2.2.10, 2.2.11, AND 2.2.23 ARE USED TO CALCULATE NOBLE GAS RELEASES FOR BWR'S.

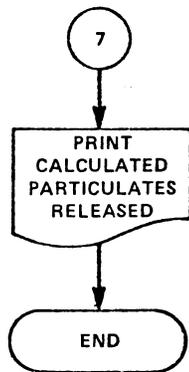


TABLE 2-14, PARAMETER 2.2.11 ARE USED TO
CALCULATE PARTICULATE RELEASES

SAMPLE BWR CASE 1

THERMAL POWER LEVEL (MEGAWATTS) 3400.00000
 PLANT CAPACITY FACTOR 0.80
 TOTAL STEAM FLOW (MILLION LBS/HR) 15.00000
 MASS OF WATER IN REACTOR VESSEL (MILLION LBS) 0.38000
 FISSION PRODUCT CARRY-OVER FRACTION 0.0010
 HALOGEN CARRY-OVER FRACTION 0.0200
 CLEAN-UP DEMINERALIZER FLOW (MILLION LBS/HR) 0.13000
 CONDENSATE DEMINERALIZER REGENERATION TIME (DAYS) 56.00000
 FRACTION FEED WATER THROUGH CONDENSATE DEMIN 1.00000

LIQUID WASTE INPUTS

STREAM	FLOW RATE (GAL/DAY)	FRACTION OF PCA	FRACTION DISCHARGED	COLLECTION TIME (DAYS)	DECAY TIME (DAYS)	I	CS	OTHERS
HIGH PURITY WASTE	2.86E+04	0.150	0.010	1.000	0.070	1.00E+03	1.00E+02	1.00E+03
LOW PURITY WASTE	5.70E+03	0.130	1.000	3.100	0.600	1.00E+03	1.00E+04	1.00E+04
CHEMICAL WASTE	6.00E+02	0.020	1.000	3.100	0.600	1.00E+03	1.00E+04	1.00E+04
REGENERANT SOLS	1.70E+03		1.000	9.400	0.440	1.00E+04	1.00E+05	1.00E+05

GASEOUS WASTE INPUTS

GLAND SEAL STEAM FLOW (THOUSAND LBS/HR) 0.0
 GLAND SEAL HOLDUP TIME (HOURS) 0.0
 AIR EJECTOR OFFGAS HOLDUP TIME (HOURS) 0.16700
 CONTAINMENT BLDG IODINE RELEASE FRACTION 0.10000
 CONTAINMENT BLDG IODINE RELEASE FRACTION 0.01000
 TURBINE BLDG. IODINE RELEASE FRACTION 1.00000
 TURBINE BLDG. PARTICULATE RELEASE FRACTION 1.00000
 GLAND SEAL VENT, IODINE PF 0.0
 AIR EJECTOR OFFGAS IODINE PF 1.00000
 AUXILIARY BLDG. IODINE RELEASE FRACTION 1.00000
 RADWASTE BLDG. PARTICULATE RELEASE FRACTION 1.00000
 RADWASTE BLDG. PARTICULATE RELEASE FRACTION 0.01000
 THERE IS A CHARCOAL DELAY SYSTEM
 KRYPTON HOLDUP TIME (DAYS) 2.66823
 XENON HOLDUP TIME (DAYS) 61.24234
 KRYPTON DYNAMIC ADSORPTION COEFFICIENT (CM3/GM) 105.00000
 XENON DYNAMIC ADSORPTION COEFFICIENT (CM3/GM) 2410.00000
 MASS OF CHARCOAL (THOUSAND LBS) 48.00000

SAMPLE BWR CASE 1 LIQUID EFFLUENTS

NUCLIDE	HALF-LIFE (DAYS)	CORROSION AND ACTIVATION PRODUCTS	CONCENTRATION IN PRIMARY COOLANT (MICRO CI/ML)				ANNUAL RELEASES TO DISCHARGE CANAL				TOTAL LWS (CURIES)	ADJUSTED TOTAL (CI/YR)	DETERGENT WASTES (CI/YR)	TOTAL (CI/YR)
			HAZARDOUS	LOW PURITY	HIGH PURITY	CHEMICAL	LOW PURITY	CHEMICAL	HIGH PURITY	CHEMICAL				
NA 24	6.25E+01	9.18E-03	0.00030	0.00014	0.00000	0.00000	0.00044	0.00155	0.0	0.00160	0.00020	0.00020	0.00020	
P 32	1.43E+01	1.81E-04	0.00001	0.00002	0.00003	0.00003	0.00006	0.00020	0.0	0.00020	0.0	0.00020	0.00020	
CR 51	2.78E+01	5.44E-03	0.00032	0.00053	0.00177	0.00177	0.00262	0.00918	0.0	0.00918	0.0	0.00918	0.00918	
MN 54	3.03E+02	6.35E-05	0.00000	0.00001	0.00004	0.00004	0.00006	0.00019	0.00100	0.00120	0.0	0.00120	0.00120	
MN 56	1.07E+01	4.74E-02	0.00028	0.00001	0.00000	0.00000	0.00028	0.00099	0.0	0.00099	0.0	0.00099	0.00099	
FE 55	9.50E+02	9.07E-04	0.00005	0.00009	0.00068	0.00068	0.00082	0.00289	0.0	0.00290	0.0	0.00290	0.00290	
FE 59	4.50E+01	2.72E-05	0.00000	0.00000	0.00001	0.00001	0.00013	0.00044	0.0	0.00044	0.0	0.00044	0.00044	
CO 58	7.13E+03	1.81E-04	0.00001	0.00002	0.00010	0.00010	0.00013	0.00044	0.00400	0.00440	0.0	0.00440	0.00440	
CU 64	1.92E+03	3.63E-04	0.00002	0.00004	0.00028	0.00028	0.00033	0.00117	0.00870	0.00990	0.0	0.00990	0.00990	
CN 65	5.33E-01	2.76E-02	0.00084	0.00032	0.00001	0.00001	0.00116	0.00406	0.0	0.00410	0.0	0.00410	0.00410	
ZN 69M	2.45E+02	1.81E-04	0.00001	0.00002	0.00013	0.00013	0.00015	0.00054	0.0	0.00054	0.0	0.00054	0.00054	
ZN 69	5.75E-01	1.84E-03	0.00006	0.00002	0.00000	0.00000	0.00008	0.00029	0.0	0.00029	0.0	0.00029	0.00029	
ZR 95	3.96E-02	0.0	0.00006	0.00003	0.00000	0.00000	0.00009	0.00031	0.0	0.00031	0.0	0.00031	0.00031	
NB 95	6.50E+01	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.00140	0.00140	0.0	0.00140	0.00140	
WI87	9.96E-01	2.74E-04	0.00001	0.00001	0.00000	0.00000	0.00002	0.00007	0.0	0.00007	0.0	0.00007	0.00007	
NP239	2.35E+00	6.37E-03	0.00032	0.00036	0.00002	0.00002	0.00070	0.00246	0.0	0.00246	0.0	0.00246	0.00246	
FISSION PRODUCTS														
BR 83	1.00E-01	3.45E-03	0.00002	0.00000	0.00000	0.00000	0.00002	0.00007	0.0	0.00007	0.0	0.00007	0.00007	
SR 89	5.20E+01	9.07E-05	0.00001	0.00001	0.00004	0.00004	0.00006	0.00020	0.0	0.00020	0.0	0.00020	0.00020	
SR 90	1.03E+04	6.35E-06	0.00000	0.00000	0.00000	0.00000	0.00001	0.00002	0.0	0.00002	0.0	0.00002	0.00002	
Y 90	2.67E+00	0.0	0.00000	0.00000	0.00000	0.00000	0.00001	0.00002	0.0	0.00002	0.0	0.00002	0.00002	
SR 91	4.03E-01	3.69E-03	0.00009	0.00003	0.00000	0.00000	0.00012	0.00042	0.0	0.00042	0.0	0.00042	0.00042	
Y 91M	3.47E-02	0.0	0.00006	0.00002	0.00001	0.00001	0.00007	0.00026	0.0	0.00026	0.0	0.00026	0.00026	
Y 91	5.88E+01	3.63E-05	0.00000	0.00001	0.00003	0.00003	0.00004	0.00014	0.0	0.00014	0.0	0.00014	0.00014	
SR 92	1.13E-01	1.47E-03	0.00016	0.00001	0.00000	0.00000	0.00006	0.00021	0.0	0.00021	0.0	0.00021	0.00021	
Y 92	1.47E-01	5.64E-03	0.00004	0.00001	0.00000	0.00000	0.00015	0.00051	0.0	0.00051	0.0	0.00051	0.00051	
Y 93	4.25E-01	3.69E-03	0.00010	0.00003	0.00000	0.00000	0.00012	0.00044	0.0	0.00044	0.0	0.00044	0.00044	
ZR 95	6.50E+01	7.26E-06	0.00000	0.00000	0.00000	0.00000	0.00001	0.00002	0.0	0.00002	0.0	0.00002	0.00002	
NB 95	3.50E+01	1.26E-06	0.00000	0.00000	0.00000	0.00000	0.00001	0.00002	0.0	0.00002	0.0	0.00002	0.00002	
NB 98	3.5E-02	3.89E-03	0.00000	0.00000	0.00000	0.00000	0.00001	0.00002	0.0	0.00002	0.0	0.00002	0.00002	
MD 99	2.79E+00	1.82E-03	0.00009	0.00011	0.00001	0.00001	0.00022	0.00076	0.0	0.00076	0.0	0.00076	0.00076	
TC 99M	2.50E-01	1.86E-02	0.00037	0.00015	0.00001	0.00001	0.00053	0.00185	0.0	0.00185	0.0	0.00185	0.00185	
RU103	3.96E+01	1.87E-05	0.00000	0.00000	0.00001	0.00001	0.00001	0.00004	0.00014	0.00014	0.0	0.00014	0.00014	
RH103M	3.96E-02	0.0	0.00000	0.00000	0.00001	0.00001	0.00001	0.00004	0.0	0.00004	0.0	0.00004	0.00004	
RU105	1.85E-01	0.0	0.00000	0.00000	0.00000	0.00000	0.00002	0.00008	0.0	0.00008	0.0	0.00008	0.00008	
RH105M	5.21E-04	1.87E-04	0.00002	0.00000	0.00000	0.00000	0.00002	0.00008	0.0	0.00008	0.0	0.00008	0.00008	
RU106	1.50E+00	2.72E-06	0.00000	0.00000	0.00000	0.00000	0.00000	0.00001	0.00014	0.00014	0.0	0.00014	0.00014	
RH106	3.67E+02	9.07E-07	0.00000	0.00000	0.00000	0.00000	0.00000	0.00001	0.00044	0.00044	0.0	0.00044	0.00044	
AG110M	2.53E+02	3.63E-05	0.00000	0.00000	0.00001	0.00001	0.00002	0.00007	0.0	0.00007	0.0	0.00007	0.00007	
TE129M	3.40E+01	0.0	0.00000	0.00000	0.00000	0.00000	0.00001	0.00004	0.0	0.00004	0.0	0.00004	0.00004	
TE129	4.79E-02	0.0	0.00000	0.00000	0.00000	0.00000	0.00001	0.00004	0.0	0.00004	0.0	0.00004	0.00004	
TE131M	1.25E+00	9.13E-05	0.00000	0.00000	0.00000	0.00000	0.00001	0.00004	0.0	0.00004	0.0	0.00004	0.00004	
I131	8.05E+00	1.60E-03	0.00009	0.00137	0.02165	0.02165	0.02311	0.08113	0.00006	0.08113	0.0	0.08113	0.08113	
I132	9.58E-02	3.68E-02	0.00017	0.00002	0.00000	0.00000	0.00019	0.00068	0.0	0.00068	0.0	0.00068	0.00068	
I133	8.75E-01	2.26E-01	0.00088	0.00535	0.00012	0.00012	0.00634	0.02226	0.0	0.02226	0.0	0.02226	0.02226	
I134	3.67E-02	7.05E-02	0.00006	0.00000	0.00000	0.00000	0.00006	0.00021	0.0	0.00021	0.0	0.00021	0.00021	
CS134	7.49E+02	2.72E-05	0.00002	0.00000	0.00000	0.00000	0.00003	0.00011	0.01300	0.01300	0.0	0.01300	0.01300	
I135	2.79E-01	2.46E-02	0.00045	0.00074	0.00001	0.00001	0.00120	0.00422	0.0	0.00422	0.0	0.00422	0.00422	
CS136	1.30E+01	7.26E-05	0.00004	0.00001	0.00001	0.00001	0.00005	0.00019	0.0	0.00019	0.0	0.00019	0.00019	

SAMPLE BWR CASE 1 LIQUID EFFLUENTS (CONTINUED)

NUCLIDE	HALF-LIFE (DAYS)	CONCENTRATION IN PRIMARY COOLANT (MICRO CI/ML)	ANNUAL RELEASES TO DISCHARGE CANAL			TOTAL LWS (CURIES)	ADJUSTED TOTAL (CI/YR)	DETERGENT WASTES (CI/YR)	TOTAL (CI/YR)
			HIGH PURITY (CURIES)	LOW PURITY (CURIES)	CHEMICAL (CURIES)				
CS137	1.10E+04	1.81E-05	0.00001	0.00000	0.00001	0.00002	0.00007	0.02400	
BA137M	1.77E-03	0.0	0.00001	0.00000	0.00001	0.00002	0.00007	0.00007	
CS138	2.24E-02	9.88E-03	0.00002	0.00000	0.00000	0.00002	0.00008	0.00008	
BA139	5.76E-02	9.62E-03	0.00002	0.00000	0.00000	0.00002	0.00007	0.00007	
BA140	1.28E+01	3.63E-04	0.00002	0.00003	0.00005	0.00011	0.00037	0.00037	
LA140	1.67E+00	0.0	0.00000	0.00002	0.00006	0.00011	0.00029	0.00029	
LA141	1.62E-01	0.0	0.00001	0.00000	0.00000	0.00001	0.00003	0.00003	
CE141	3.24E+01	2.72E-05	0.00000	0.00000	0.00000	0.00002	0.00006	0.00006	
LA142	6.39E-02	4.80E-03	0.00001	0.00000	0.00000	0.00001	0.00005	0.00005	
PR143	1.37E+01	3.63E-05	0.00000	0.00000	0.00001	0.00001	0.00004	0.00004	
CE144	2.84E+02	2.72E-06	0.00000	0.00000	0.00000	0.00000	0.00001	0.00001	
ALL OTHERS		1.98E-01	0.00001	0.00000	0.00001	0.00002	0.00006	0.00006	
TOTAL (EXCEPT TRITIUM)		5.29E-01	0.00513	0.00953	0.02517	0.03983	0.13983	0.06234	0.20000

TRITIUM RELEASE 26 CURIES PER YEAR

SAMPLE BWR CASE 1

BWR

THERMAL POWER LEVEL (MEGAWATTS) 3400.00000
 PLANT CAPACITY FACTOR 0.80
 TOTAL STEAM FLOW (MILLION LBS/HR) 15.00000
 MASS OF WATER IN REACTOR VESSEL (MILLION LBS) 0.38000
 CLEAN-UP DEMINERALIZER FLOW (MILLION LBS/HR) 0.13000
 CONDENSATE DEMINERALIZER REGENERATION TIME (DAYS) 56.00000
 FRACTION FEED WATER THROUGH CONDENSATE DEMIN 1.00000
 REACTOR VESSEL HALOGEN CARRYOVER FACTOR 0.01500

LIQUID WASTE INPUTS

STREAM	FLOW RATE (GAL/DAY)	FRACTION OF PCA DISCHARGED	FRACTION COLLECTION TIME (DAYS)	DECAY TIME (DAYS)	DECONTAMINATION FACTORS
HIGH PURITY WASTE	2.86E+04	0.150	0.010	0.070	I 1.00E+03 CS 1.00E+02 OTHERS 1.00E+03
LOW PURITY WASTE	5.70E+03	0.130	1.000	0.600	1.00E+03 1.00E+04 1.00E+04 1.00E+04
CHEMICAL WASTE	6.00E+02	0.020	1.000	0.600	1.00E+03 1.00E+04 1.00E+05 1.00E+05
REGENERANT SOLS	1.70E+03	1.000	9.400	0.440	1.00E+04 1.00E+05 1.00E+05 1.00E+05

GASEOUS WASTE INPUTS

GLAND SEAL STEAM FLOW (THOUSAND LBS/HR) 0.0
 GLAND SEAL HOLDUP TIME (HOURS) 0.0
 AIR EJECTOR OFFGAS HOLDUP TIME (HOURS) 0.16700
 CONTAINMENT BLDG IODINE RELEASE FRACTION 0.10000
 PARTICULATE RELEASE FRACTION 0.01000
 TURBINE BLDG. IODINE RELEASE FRACTION 1.00000
 PARTICULATE RELEASE FRACTION 1.00000
 GLAND SEAL VENT, IODINE PF 1.00000
 AIR EJECTOR OFFGAS IODINE PF 1.00000
 AUXILIARY BLDG. IODINE RELEASE FRACTION 1.00000
 PARTICULATE RELEASE FRACTION 1.00000
 RADWASTE BLDG. IODINE RELEASE FRACTION 0.01000
 PARTICULATE RELEASE FRACTION 0.01000

THERE IS A CHARCOAL DELAY SYSTEM

KRYPTON HOLDUP TIME (DAYS) 2.66823
 XENON HOLDUP TIME (DAYS) 61.24234
 KRYPTON DYNAMIC ADSORPTION COEFFICIENT (CM3/GM) 105.00000
 XENON DYNAMIC ADSORPTION COEFFICIENT (CM3/GM) 2410.00000
 MASS OF CHARCOAL (THOUSAND LBS) 48.00000

SAMPLE BWR CASE 1

GASEOUS RELEASE RATE
(CURIES PER YEAR)

NUCLIDE	COOLANT CONC. (MICROCURIES/G)	CONTAINMENT BLDG.	TURBINE BLDG.	AUXILIARY BLDG.	RADWASTE BLDG.	GLAND SEAL	AIR EJECTOR	MECH VAC PUMP	TOTAL
I-131	1.785E-03	1.1E-03	1.1E-01	2.1E-02	1.1E-02	0.0	0.0	8.2E-02	2.3E-01
I-133	2.499E-02	1.5E-02	1.6E+00	2.9E-01	1.5E-01	0.0	0.0	9.2E-01	3.0E+00

H-3 RELEASED FROM TURBINE BLDG. VENTILATION SYSTEM 2.6E+01

H-3 RELEASED FROM CONTAINMENT BLDG. VENTILATION SYSTEM 2.6E+01

TOTAL H-3 RELEASED VIA GASEOUS PATHWAY 5.2E+01

C-14 RELEASED VIA MAIN CONDENSER OFFGAS SYSTEM = 9.5 CI/YR

SAMPLE BWR CASE 1

GASEOUS RELEASE RATE
(CURIES PER YEAR)

NUCLIDE	COOLANT CONC. (MICROCURIIES/G)	CONTAINMENT BLDG.	TURBINE BLDG.	AUXILIARY BLDG.	RADWASTE BLDG.	GLAND SEAL	AIR EJECTOR	MECH VAC PUMP	TOTAL
AR-41	0.0	1.5E+01	0.0	0.0	0.0	0.0	2.3E+01	0.0	3.8E+01
KR-83M	9.100E-03	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
KR-85M	1.600E-03	1.0E+00	2.5E+01	3.0E+00	0.0	0.0	3.0E+00	0.0	3.2E+01
KR-85	5.000E-06	0.0	0.0	0.0	0.0	0.0	2.4E+02	0.0	2.4E+02
KR-87	5.500E-03	0.0	6.1E+01	2.0E+00	0.0	0.0	0.0	0.0	6.3E+01
KR-88	5.500E-03	1.0E+00	9.1E+01	3.0E+00	0.0	0.0	0.0	0.0	9.5E+01
KR-89	3.400E-02	0.0	5.8E+02	2.0E+00	2.9E+01	0.0	0.0	0.0	6.1E+02
XE-131M	3.900E-06	0.0	0.0	0.0	0.0	0.0	5.0E+00	0.0	5.1E+00
XE-133M	7.500E-05	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
XE-133	2.100E-03	2.7E+01	1.5E+02	8.3E+01	2.2E+02	0.0	3.2E+01	1.3E+03	1.8E+03
XE-135M	7.000E-03	1.5E+01	4.0E+02	4.5E+01	5.3E+02	0.0	0.0	0.0	9.9E+02
XE-135	6.000E-03	3.3E+01	3.3E+02	9.4E+01	2.8E+02	0.0	0.0	5.0E+02	1.2E+03
XE-137	3.900E-02	4.5E+01	1.0E+03	1.4E+02	8.3E+01	0.0	0.0	0.0	1.3E+03
XE-138	2.300E-02	2.0E+00	1.0E+03	6.0E+00	2.0E+00	0.0	0.0	0.0	1.0E+03
TOTAL NOBLE GASES									7.4E+03

0.0 APPEARING IN THE TABLE INDICATES RELEASE IS LESS THAN 1.0 CI/YR FOR NOBLE GAS

SAMPLE BWR CASE 1

AIRBORNE PARTICULATE RELEASE RATE

(CURIES PER YEAR)

NUCLIDE	CONTAINMENT					TURBINE BLDG.			AUXILIARY BLDG.			RADWASTE BLDG.		MECH VAC. PUMP	TOTAL
	BLDG.					BLDG.			BLDG.						
CR-51	2.0E-06	9.0E-04	9.0E-04	7.0E-06	1.0E-06	1.0E-06									1.8E-03
MN-54	4.0E-06	6.0E-04	1.0E-03	4.0E-05	0.0										1.6E-03
CO-58	1.0E-06	1.0E-03	2.0E-04	2.0E-06	0.0										1.2E-03
FE-59	9.0E-07	1.0E-04	3.0E-04	3.0E-06	0.0										4.0E-04
CO-60	1.0E-05	1.0E-03	4.0E-03	7.0E-05	5.6E-07										5.1E-03
ZN-65	1.0E-05	6.0E-03	4.0E-03	3.0E-06	3.4E-07										1.0E-02
SR-89	3.0E-07	6.0E-03	2.0E-05	0.0	0.0										6.0E-03
SR-90	3.0E-08	2.0E-05	7.0E-06	0.0	0.0										2.7E-05
NB-95	1.0E-05	6.0E-06	9.0E-03	4.0E-08	0.0										9.0E-03
ZR-95	3.0E-06	4.0E-05	7.0E-04	8.0E-06	0.0										7.5E-04
MO-99	6.0E-05	2.0E-03	6.0E-02	3.0E-08	0.0										6.2E-02
RU-103	2.0E-06	5.0E-05	4.0E-03	1.0E-08	0.0										4.1E-03
AG-110M	4.0E-09	0.0	2.0E-06	0.0	0.0										2.0E-06
SB-124	2.0E-07	1.0E-04	3.0E-05	7.0E-07	0.0										1.3E-04
CS-134	7.0E-06	2.0E-04	4.0E-03	2.4E-05	3.2E-06										4.2E-03
CS-136	1.0E-06	1.0E-04	4.0E-04	0.0	1.9E-06										5.0E-04
CS-137	1.0E-05	1.0E-03	5.0E-03	4.0E-05	8.9E-06										6.1E-03
BA-140	2.0E-05	1.0E-02	2.0E-02	4.0E-08	1.1E-05										3.0E-02
CE-141	2.0E-06	1.0E-02	7.0E-04	7.0E-08	0.0										1.1E-02

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1. C GALE CODE FOR CALCULATING LIQUID EFFLUENTS FROM LWRS. MODIFIED
2. C OCT. 1978 TO IMPLEMENT APPENDIX I TO 10 CFR PART 50. REACTOR
3. C WATER CONCENTRATIONS CALCULATED USING METHODS OF DRAFT STANDARD
4. C ANS 237 'RADIOACTIVE MATERIALS IN PRINCIPAL FLUID STREAMS OF
5. C LIGHT WATER COOLED NUCLEAR POWER PLANTS' DRAFT DATED MAY 20, 1974
6. C MODIFIED EDITION OF ORIGEN PROGRAM TO COMPUTE EFFLUENTS FROM BWR
7. C AND PWR RADWASTE SYSTEMS
8. C
9. C LOGICAL DISCHG, POWRIT
10. C INTEGER*2 LOC, NON0, KD
11. C REAL*4 LETDWN, NOGEN
12. C REAL*4 LETDWA
13. C REAL KKR, KXE, KNO, KMASS
14. C INTEGER*2 NAME(3)
15. C COMMON/MATRIX/A(2500), LOC(2500), NON0(800), KD(800)
16. C COMMON/FLEX/FLUX(10), MMN, MOUT, INDEX, QXN, AXN, ERR, NOBLND, MZERO
17. C COMMON/PROCS/ MPROS(8), NOPROS(8), NZPROS(8,20), PR(800)
18. C COMMON/EQ/XZERO(800), XZH(800), XTEMP(800), XNEW(10,800),
19. C B(800), D(800)
20. C COMMON/FLUXN/T(20), POWER(10), TOCAP(800), FISS(100), DIS(800), ILITE,
21. C IACT, IEP, ITOT, NON, INPT
22. C COMMON/OUT/NUCL(800), TITLE(20), Q(800), FG(800), CUTOFF(7),
23. C POW, BURNUP, FLUXB, MSTAR, ALPHAN(100), SPONF(100), ABUND(500),
24. C BASIS(10), TCONST, TUNIT
25. C COMMON/CONC/PCONC(800), DWCONC(800), CMCONC(800),
26. C SCON(800), RINV(800)
27. C COMMON/COOL/REACTR, POW1, TYPE, PCVOL, LETDWN, NDGAS, SCVOL, STMVOL, NOGEN
28. C , NPURGE, NVCSPG, SBLDR, GASDLA, STLKR, BLMDWN, EJCTR, WLKRAT,
29. C GASLKR, CONDLR, DEBDM, DFCSBDM, NZMBDM, NZCBDM, NE, PF,
30. C STMPR, FPEF, HEF, FFCSDM, DFBCS, CBFLR, DFI, DFCS, DF,
31. C EDFLR, DFIED, DFCS, DFED, DWFELR, DFIDW, DFCS, DFDW, DILUT
32. C , SBA, EDA, DWA, CWFLR, CMWFR, CMA, DFCM, DFICM, DFCS,
33. C DFICW, DFICW, DFCS, MHLDB, MHLDB, MHLDB, MHLDB, MHLDB,
34. C , BDTFR, DFIBD, DFCS, DFBD, MHLDB, MHLDB, MHLDB, MHLDB,
35. C SBFD, DFMO, DFY, EDFD, DFMOED, DFYED, DWF, DFMODW, DFYDW,
36. C DFMOBD, DFYBD, CMFD, DFMOCW, DFYCW, CMFD, DFMOCM, DFYCM
37. C A , TS, TE, TD, TB, TC, TCM, TSTORC, TSTORD, TSTORB, TMSC, DWFL2, DW2, DWF2,
38. C T2, TSTOR2, DFID2, DFCS, DFOD2, DFYD2, DFYD2, PFLAUN
39. C COMMON/APCOOL/RGWER, DFIRG, DFCSRG, DFRG, TRG, TSTORR, RGFD
40. C COMMON/BDTES/RFNRT
41. C COMMON /CONB/BCONC(800)
42. C DIMENSION WORD13(4), WORD15(4), WORD18(5), WORD23(6), WORD28(7),
43. C WORD33(9), WORD40(10)
44. C DIMENSION REACTR(7), NZMBDM(26), NZCBDM(26)
45. C DIMENSION FACT(10), XCOMP(20), INUCL(20)
46. C DIMENSION WORD56(14)
47. C DATA YES, 'YES',
48. C FOLLOWING ISOTOPES WITH THEIR CONCENTRATIONS IN UCI/GM) ARE
49. C ALSO PRESENT IN THE PRIMARY COOLANT BUT ARE NOT CONSIDERED
50. C SIGNIFICANT IN EFFLUENT CALCULATIONS: N-13, .05; N-16, .60; N-17, .009;
51. C O-19, .7; F-18, .004.
52. C READ NUCLEAR DATA AND CONSTRUCT TRANSITION MATRIX
53. C
54. C CALL NUDATA(NLIBE)
55. C
56. C DO 20 I=2, ITOT
57. C NON0(I)=NON0(I)+NON0(I-1)
58. C KD(I)=KD(I)+NON0(I-1)
59. C DISCHG=.FALSE.
60. C POWRIT=.FALSE.

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61. KT=0
62. INDEX=0
63. FLXB=0.0
64. PARH=0.0
65. BURN=0.0
66. BDTFR=1.0
67. QXN=0.001
68. AXN=-ALOG(QXN)
69. NE=ITOT
70. TCONST=86400.
71. MMN=0
72. MZERO=21
73. EDA=0.0
74. TMSC=0.0
75. TE=0.0
76. TS=0.0
77. T2=0.0
78. TSTOR2=0.0
79. DWFL2=0.0
80. DW2=0.0
81. DWF2=0.0
82. DO 40 J=1,800
83. PCONC(J)=0.0
84. DWCONC(J)=0.0
85. SCON(J)=0.0
86. RINV(J)=0.0
87. CWCONC(J)=0.0
88. CMCONC(J)=0.0
89. XZH(J)=0.0
90. 40 CONTINUE
91.
92. C READ DESCRIPTION OF REACTOR AND RADWASTE TREATMENT PLANT
93. C
94. C
95. C
96. C
97. C
98. C
99. C
100. C
101. C
102. C
103. C
104. C
105. C
106. C
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111. C
112. C
113. C
114. C
115. C
116. C
117. C
118. C
119. C
120. C

PRINT 9026
READ 9010,REACTR,TYPE
PRINT 9010,REACTR,TYPE
READ 9022,WORD56,POW1
PRINT 9022,WORD56,POW1
PF=0.80
PRINT 9027

READ DATA FOR BWR LIQUID CODE
50 READ 9022,WORD56,STMFR
PRINT 9022,WORD56,STMFR
READ 9022,WORD56,PCVOL
PRINT 9022,WORD56,PCVOL
FPEF=0.001
HEF=0.020
PRINT 9030,FPEF,HEF
READ 9022,WORD56,LETDWN
PRINT 9022,WORD56,LETDWN
PC = 0.015
READ 9022,WORD56,REGENT
IF(REGENT.EQ.0.0) PC = 0.004
PRINT 9022,WORD56,REGENT
READ 9022,WORD56,FFCDM
PRINT 9022,WORD56,FFCDM
PRINT 9045
READ 9013,WORD18,CWFLR,WORD8,CWA

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121. READ 9014,DFICW,DFCSCW,DFCW
122. READ 9015,TC,TSTORC,CWFD
123. PRINT 9016
124. PRINT 9017,WORD18,CWFLR,CWA,CWFD,TC,TSTORC,DFICW,DFCSCW,DFCW
125. READ 9013,WORD18,DWFLR,WORD8,DWA
126. READ 9014,DFIDW,DFCSDW,DFDW
127. READ 9015,TD,TSTORD,DWFD
128. PRINT 9017,WORD18,DWFLR,DWA,DWFD,TD,TSTORD,DFIDW,DFCSDW,DFDW
129. READ 9013,WORD18,CWFLR,WORD8,CMA
130. READ 9014,DFICM,DFCSCM,DFCM
131. READ 9015,TCM,TSTORB,CMFD
132. PRINT 9017,WORD18,CWFLR,CMA,CMFD,TCM,TSTORB,DFICM,DFCSCM,DFCM
133. READ 9037,RGWFR
134. READ 9014,DFIRG,DFCSR,DFRG
135. READ 9015,TRG,TSTORR,RGFD
136. PRINT 9038,RGWFR,RGFD,TRG,TSTORR,DFIRG,DFCSR,DFRG
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READ DATA FOR BWR GAS CODE

PRINT 9046
READ 9022,WORD56,GG5
PRINT 9022,WORD56,GG5
READ 9022,WORD56,TIM3
PRINT 9022,WORD56,TIM3
READ 9022,WORD56,TIM4
PRINT 9022,WORD56,TIM4
HEPA1=1.0
FIL1=1.0
HEPA2=1.0
FIL2=1.0
HEPA5=1.0
FIL5=1.0
HEPA6=1.0
FIL6=1.0
FILGS = 1.0
FILEJ = 1.0
READ 9060,WORD15,CBCH,CBHEPA
IF(CBCH.GT.0.0)FIL1 = (1.0 - CBCH/100.)
IF(CBHEPA.GT.0.0)HEPA1 = (1.0 - CBHEPA/100.)
PRINT 9061,WORD15,FIL1,HEPA1
READ 9062,WORD15,IBCH,IBHEPA
IF(TBCH.GT.0.0)FIL2 = (1.0 - TBCH/100.)
IF(TBHEPA.GT.0.0)HEPA2 = (1.0 - TBHEPA/100.)
PRINT 9063,WORD15,FIL2,HEPA2
READ 9022,WORD56,FIL3
IF(FIL3.GT.0.0)FILGS = (1.0 - FIL3/100.)
PRINT 9022,WORD56,FILGS
READ 9022,WORD56,FIL4
IF(FIL4.EQ.1.0)FILEJ = (1.0 - FIL4)
IF(FIL4.GT.1.0)FILEJ = (1.0 - FIL4/100.)
IF(FIL4.EQ.0.0)FILEJ = 1.0
PRINT 9022,WORD56,FILEJ
READ 9060,WORD15,AXCH,AXHEPA
IF(AXCH.GT.0.0)FIL5 = (1.0 - AXCH/100.)
IF(AXHEPA.GT.0.0)HEPA5 = (1.0 - AXHEPA/100.)
PRINT 9061,WORD15,FIL5,HEPA5
READ 9060,WORD15,RWCH,RWHEPA
IF(RWCH.GT.0.0)FIL6 = (1.0 - RWCH/100.)
IF(RWHEPA.GT.0.0)HEPA6 = (1.0 - RWHEPA/100.)
PRINT 9061,WORD15,FIL6,HEPA6

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181. READ 9021,KCHAR
182. READ 9022,WORD56,KKR
183. READ 9022,WORD56,KXE
184. READ 9022,WORD56,KMASS
185. READ 9020,WORD56,PFLAUN
186. IF(KCHAR.EQ.0) GO TO 54
187. IF(KCHAR.EQ.1) GO TO 55
188. PRINT 9023
189. GO TO 56
190. PRINT 9024
191. GO TO 56
192. 54 CHTI1 = 1.8 * (KMASS * KKR)/POM1
193. CHTI2 = 1.8 * (KMASS * KXE)/POM1
194. PRINT 9025,CHTI1,CHTI2,KKR,KXE,KMASS
195. 56 CONTINUE
196. IF(PFLAUN.EQ.0.0) GO TO 99
197. GO TO 98
198. CONTINUE
199. PRINT 9048
200. 98 CONTINUE
201. PRINT 9026
202. 57 DO 58 I=1,ITOT
203. B(I)=0.0
204. CONTINUE
205. DFIED=1.
206. DFSED=1.
207. DFED=1.
208. DFID2=1.
209. DFCS2=1.
210. DFD2=1.
211.
212.
213.
214. C
215. C CALCULATE BWR PRIMARY COOLANT CONCENTRATIONS
216. DO 2251 I=1,ITOT
217. PCONC(I)=BONC(I)
218. POWA=POW1
219. PCVOA=PCVOL*1E6
220. LETDWA=LETDWN*1E6
221. STMFA=STMFR*1E6
222. FFCDA=FFCDM
223. CHECK TO SEE IF PLANT PARAMETERS ARE WITHIN SPECIFIED RANGES
224. IF(FFCDA.LT.0.99) FFCDA=0.18
225. IF(ABS(PCVOA-3400).GT.400.1)GO TO 252
226. IF(ABS(PCVOA-3.8E5).GT.0.4001E5)GO TO 252
227. IF(ABS(LETDWA-1.5E7).GT.0.2001E7)GO TO 252
228. IF(ABS(STMFA-1.5E7).GT.0.2001E7)GO TO 252
229. GO TO 256
230. C
231. C CALCULATE BWR ADJUSTMENT FACTORS
232. RHAL2=(LETDWA*0.9+FFCDA*STMFA*PC*0.9)/PCVOA
233. IF(FFCDA.GT.0.99) GO TO 299
234. FFCDA = 0.01
235. 299 CONTINUE
236. RCSR2=(LETDWA*0.5+FFCDA*STMFA*5E-4)/PCVOA
237. RCFP2=(LETDWA*0.9+FFCDA*STMFA*9E-4)/PCVOA
238. RK2=111.76*POWA/PCVOA
239. DO 255 J=1,ITOT
240. IF(PCONC(J).EQ.0.0) GO TO 255
241. NZ=NUCL(J)/10000
242. DL=DIS(J)*3600
243. IF (NZ.EQ.53.OR.NZ.EQ.35)GO TO 253
244.
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241. IF (NZ.EQ.37.OR.NZ.EQ.55)GO TO 254
242. PCONC(J)=PCONC(J)*RK2*(0.3114+DL)/(RCFF2+DL)
243. GO TO 255
244. PCONC(J)=PCONC(J)*RK2*(0.3612+DL)/(RHAL2+DL)
245. GO TO 255
253 PCONC(J)=PCONC(J)*RK2*(0.1730+DL)/(RCSR2+DL)
254 CONTINUE
255 PCVOL=PCVOL*100000./62.4
256 LETDN=LETDN*2000.
257 STMR=STMR*2851.
258 DO 2255 J=1,ITOT
259 IF (PCONC(J).GT.0.0)PCONC(J)=PCONC(J)/(DIS(J)*1.6283E13)
2255 CONTINUE
IF(REGENT.GT.0.0) GO TO 257
CALL EFFTAB
GO TO 30

C
C COMPUTE REMOVAL CONSTANT FOR CONDENSATE DEMINERALIZER IN BMR
257 FFCDM = FFCDA
IF(FFCDM.EQ.0.1) GO TO 300
GO TO 301
300 FFCDM = 0.01
301 CONTINUE
CCBDM=0.9*STMR*FPEF/(PCVOL*7.48*60.)*FFCDM
CSBDM=0.5*STMR*FPEF/(PCVOL*7.48*60.)*FFCDM
IF(FFCDM.EQ.0.01) GO TO 304
CCBDI = CCBDM
GO TO 305
304 CONTINUE
FFCDM = 0.1
CCBDI = 0.9*STMR*FPEF/(PCVOL*7.48*60.)*FFCDM
CONTINUE
DO 258 I=1,ITOT
NZ=NUCL(I)/10000
PR(I)=CCBDM
IF(NZ.EQ.53.OR.NZ.EQ.35)PR(I)=CCBDI*HEF/FPEF
IF(NZ.EQ.37.OR.NZ.EQ.55)PR(I)=CSBDM
XZHI=PCONC(I)*PR(I)*PCVOL*0.02832
B(I)=XZHI
XZH(I)=XZHI*86400.
258 CONTINUE
XZERO(I)=0.
CALCULATE INVENTORIES ON BWR CONDENSATE RESINS
290 T(1)=REGENT
CALL SOLVE
DO 295 I=1,ITOT
RINV(I)=XTEMP(I)
CALL EFFTAB
GO TO 30
FORMATS
FORMATS
C
9000 FORMAT(20A4)
9001 FORMAT(10E8.2)
9002 FORMAT(8E10.3)
9003 FORMAT(5(I6,E9.2),I5)
9004 FORMAT(16I5)
9005 FORMAT('0MMN OR MOUT EXCEEDS DIMENSIONS')
9006 FORMAT('0MOUT SHOULD NOT EXCEED MMN BY MORE THAN 10'//)
9007 FORMAT(8(E8.2,I2)

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301. 9008 FORMAT(20I4) 0001500
 302. 9009 FORMAT(10A4,F7.0,A3,F10.3) 0001505
 303. 9010 FORMAT(32X,8A4,12X,A4) 0001510
 304. 9011 FORMAT(16X,14A4,F8.4) 0001515
 305. 9012 FORMAT(15X,4A4,A2,8X,F8.0,1X,A4,A2,F5.3) 0001520
 306. 9013 FORMAT(20X,F8.0,2(5X,F8.0)) 0001525
 307. 9014 FORMAT(27X,F6.2,14X,F6.2,18X,F6.2) 0001530
 308. 9015 FORMAT(0,30X,'FRACTION COLLECTION DECAY'/8X,'STREAM
 309. 1 FLOW RATE OF PCA DISCHARGED TIME
 310. 2MINATION FACTORS',20X,'(GAL/DAY)',23X,'(DAYS)
 311. 3'I',8X,'CS',6X,'OTHERS') 0001535
 312. 9017 FORMAT(2X,4A4,A2,1PE9.2,1X,4(0PF8.3,2X),3(1PE9.2,1X)) 0001540
 313. 9020 FORMAT(16X,14A4,F8.4) 0001545
 314. 9021 FORMAT(79X,I1) 0001550
 315. 9022 FORMAT(16X,13A4,A2,F10.5) 0001555
 316. 9023 FORMAT(16X,'THERE IS A CRYOGENIC DISTILLATION COLUMN'/20X,'IODINE
 317. 1AND XENON DECONTAMINATION FACTOR',T71,'10000.'/20X,'KRYPTON DECONT
 318. 2AMINATION FACTOR',T72,'4000.'/20X,'KRYPTON AND XENON HOLDUP TIME (
 319. 3DAYS)',T74,'90.') 0001560
 320. 9024 FORMAT(16X,'THERE IS NO CHARCOAL DELAY SYSTEM') 0001565
 321. 9025 FORMAT(16X,'THERE IS A CHARCOAL DELAY SYSTEM'/20X,'KRYPTON HOLDUP
 322. 1TIME (DAYS)',T72,F9.5/20X,'XENON HOLDUP TIME (DAYS)',T72,F9.5/
 323. 220X,'KRYPTON DYNAMIC ADSORPTION COEFFICIENT (CM3/GM)',T72,F9.5/
 324. 320X,'XENON DYNAMIC ADSORPTION COEFFICIENT(CM3/GM)',T71,F10.5/20X,
 325. 4'MASS OF CHARCOAL(THOUSAND LBS)',T72,F9.5) 0001570
 326. 9026 FORMAT(1H1) 0001575
 327. 9027 FORMAT(16X,'PLANT CAPACITY FACTOR',T75,'0.80') 0001580
 328. 9028 FORMAT(16X,'PERCENT FUEL WITH CLADDING DEFECTS',T75,F6.4) 0001585
 329. 9029 FORMAT(16X,'MASS OF WATER IN STEAM GENERATORS (THOUSAND LBS)',T73,
 330. 1F8.4) 0001590
 331. 9030 FORMAT(16X,'FISSION PRODUCT CARRY-OVER FRACTION',T75,F6.4/16X,
 332. 1'HALOGEN CARRY-OVER FRACTION',T75,F6.4) 0001595
 333. 9032 FORMAT(2X,7A4,F7.0,3A4,A1,F5.3,3A4,A3,I2,2A4) 0001600
 334. 9034 FORMAT(2X,'BLOWDOWN',10X,1PE9.2,14X,0PF5.3,2X,2(F8.3,2X),
 335. 13(1PE9.2,1X)) 0001605
 336. 9035 FORMAT(2X,'UNTREATED BLOWDOWN',1PE9.2,11X,' 1.000 0.0
 337. 10.0 1.00E 00 1.00E 00 1.00E 00') 0001610
 338. 9036 FORMAT(16X,'THERE IS NOT A CONDENSATE DEMINERALIZER') 0001615
 339. 9037 FORMAT(72X,F8.2) 0001620
 340. 9038 FORMAT(2X,'REGENERANT SOLS ',1PE9.2,14X,0PF5.3,2X,2(F8.3,2X),
 341. 13(1PE9.2,1X)) 0001625
 342. 9039 FORMAT(16X,'THERE IS A CRYOGENIC OFFGAS SYSTEM') 0001630
 343. 9040 FORMAT(16X,'THERE IS NO CRYOGENIC OFFGAS SYSTEM') 0001635
 344. 9041 FORMAT(16X,'PRIMARY TO SECONDARY LEAK RATE (LBS/DAY)',T73,'100.') 0001640
 345. 9045 FORMAT ('',0 LIQUID WASTE INPUTS') 0001645
 346. 9046 FORMAT ('',0 GASEOUS WASTE INPUTS') 0001650
 347. 9048 FORMAT(0,15X,'THERE IS NOT AN ON-SITE LAUNDRY') 0001655
 348. 9051 FORMAT(16X,'BLOWDOWN RATE (THOUSAND LBS/HR)',25X,F8.4) 0001660
 349. 9052 FORMAT(16X,'THERE IS CONTINUOUS STRIPPING OF FULL LETDOWN FLOW') 0001665
 350. 9053 FORMAT(16X,'THERE IS NOT CONTINUOUS STRIPPING OF FULL LETDOWN FLOW'
 351. 1) 0001670
 352. 9054 FORMAT(16X,'FLOW RATE THROUGH GAS STRIPPER (GPM)',20X,F8.4) 0001675
 353. 9055 FORMAT(36X,F8.4,35X,I1) 0001680
 354. 9056 FORMAT(15X,4A4,A2,8X,F8.0) 0001685
 355. 9060 FORMAT(16X,4A4,10X,F4.0,6X,F4.0) 0001690
 356. 9061 FORMAT(16X,4A4,'IODINE RELEASE FRACTION',16X,F10.5/32X,'PARTICULA
 357. 1IE RELEASE FRACTION',10X,F10.5) 0001695
 358. 9062 FORMAT(16X,4A4,10X,F4.0,6X,F4.0) 0001700
 359. 9063 FORMAT(16X,4A4,'IODINE RELEASE FRACTION',16X,F10.5/32X,'PARTICULAT
 360. 1E RELEASE FRACTION',10X,F10.5) 0001705
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361. 9064 FORMAT(16X, 'STEAM LEAK TO TURBINE BLDG (LBS/HR)', 19X, F10.5)
362. 9065 FORMAT(16X, 4A4, 6X, A3)
363. 9066 FORMAT(16X, 4A4, 6X, 'PARTICULATE RELEASE FRACTION', 6X, F10.5)
364. 9067 FORMAT(16X, 5A4, 10X, A3, 6X, A3)
365. 9068 FORMAT(16X, 5A4, 'IODINE RELEASE FRACTION', 11X, F10.5/36X, 'PARTICULATE
366. 1E RELEASE FRACTION', 6X, F10.5)
367. 9069 FORMAT(16X, 5A4, 9X, F8.2, 9X, A3, 6X, A3)
368. 9070 FORMAT(16X, 5A4, 'RATE(CFM)', 27X, F8.2/16X, 5A4, 'IODINE RELEASE FRACTI
369. 10N', 11X, F10.5/36X, 'PARTICULATE RELEASE FRACTION', 6X, F10.5)
370. 9071 FORMAT(16X, 5A4, 10X, A3, 6X, A3, 19X, F3.0)
371. 9072 FORMAT(16X, 'FREQUENCY OF CNTMT BLDG HIGH VOL PURGE (TIMES/YR)',
372. 1174, F6.0)
373. 9073 FORMAT(16X, 'THERE IS NOT A CNTMT BLDG LOW VOL PURGE')
374. 9075 FORMAT(16X, 'THERE IS CONTINUOUS LOW VOL PURGE OF VOL. CONTROL TK')
375. END
376. SUBROUTINE EFFTAB
377. INTEGER*2 NAME(3)
378. INTEGER*2 LOC, NON0, KD
379. REAL*4 LETDWN, NOGEN
380. REAL*4 LETDWA
381. DIMENSION NZCBDM(26), NZCBDM(26), NZCBDM(26), REACTR(7)
382. DIMENSION TURBDR(800), DWCON2(800), EDCONC(800)
383. DIMENSION LAUNDRY(12), WLAUND(12)
384. COMMON/EQ/XZERO(800), XZH(800), XTEMP(800), XNEM(10, 800),
385. 1 B(800), D(800)
386. COMMON/FLUXN/T(20), POWER(10), TOCAP(800), FISS(100), DIS(800), ILITE,
387. 1 IACT, IFF, ITOT, NON, IHPT
388. COMMON/OUT/NUCL(800), TITLE(20), Q(800), FG(800), CUTOFF(7),
389. 1 POW, BURHUP, FLUXB, MSTAR, ALPHAN(100), SPONF(100), ABUND(500),
390. 2 BASIS(10), TCONST, TUHIT
391. COMMON/COOL/REACTR, POW1, TYPE, PCVOL, LETDWN, NDGAS, SCVOL, STMVOL, NOGEN
392. 1 , NPURGE, HVCSPG, SBLDR, GASDLA, STLKR, BLWDWN, ECTR, WLKRAT,
393. 2 GASLKR, CONDLR, DFMBDM, DFCBDM, NZMBDM, NZCBDM, NE, PF,
394. 3 STMFR, FPEF, HEF, FFCDM, DFMBCS, CBFLR, DFI, DFCS, DF,
395. 4 EDFLR, DFIED, DFCESED, DFED, DWFLR, DFIDW, DFCSDW, DFDW, DILUT
396. 5 , SBA, EDA, DNA, CWFLR, CMNFR, CWA, CMA, DFCM, DFCM, DFCSCM,
397. 6 DFCW, DFICW, DFCSCW, MHOLD, MHOLDE, MHOLDW, MHOLCM, MHOLDC
398. 7 , BDTFR, DFIBD, DFCSD, DFBD, MHOLDB, REGEN,
399. 8 SBFD, DFMD, DFY, EDFD, DFMOED, DFYED, DWFD, DFMDW, DFYDW,
400. 9 DFMOBD, DFYBD, CWFD, DFMOCW, DFYCW, CMFD, DFMOCM, DFYCM
401. A , TS, TE, TD, TB, TC, TCM, TSTORC, TSTORD, TSTORB, TMS, DNFL2, DW2, DWF2,
402. B T2, TSTOR2, DFID2, DFCSD2, DFMD2, DFYD2, DFD2, PFLAUN
403. COMMON/BDTES/RFNRT
404. COMMON/FLEX/FLUX(10), MYN, MOUT, INDEX, QXN, AXN, ERR, NOBLND, MZERO
405. COMMON/CONC/PCONC(800), DWCONC(800), CWCONC(800), CMCONC(800),
406. 1 SCON(800), RINV(800)
407. COMMON/MPC/MPCCTAB, AMPC(800), WMPG(800)
408. EQUIVALENCE (XZERO(1), TURBDR(1)), (XZH(1), DWCON2(1))
409. DATA LAUNDRY/250540, 270580, 270600, 400950, 410950, 441030, 441060,
410. 1 471101, 531310, 551340, 551370, 581440/
411. DATA WLAUND/0.001, 0.004, 0.0087, 0.0014, 0.002, 0.00014, 0.0024,
412. 1 0.00044, 0.000062, 0.013, 0.024, 0.0052/
413. DO 10 I=1, ITOT
414. D(I)=-DIS(I)
415. 10
416. H3BWR = 0.03 * POW1
417. TRITPR = H3BWR * 0.5
418. TRITCO = 0.1
419. DO 30 J=1, ITOT
420. CWCONC(J)=0.0

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421. EDCONC(J)=0.0
422. DWCONC(J)=0.0
423. DWCON2(J)=0.0
424. CMCONC(J)=0.0
425. NZ=NUCL(J)/10000
426. IF(NZ.EQ.36.OR.NZ.EQ.54) GO TO 30
427. CWCONC(J)=PCONC(J)*CWA
428. EDCONC(J)=PCONC(J)*EDA
429. DWCONC(J)=PCONC(J)*DWA
430. DWCON2(J)=PCONC(J)*DW2
431. CMCONC(J)=PCONC(J)*CMA
432. CONTINUE
30
C
C
C
C
CALCULATE RADIOACTIVITY AFTER COLLECTION AT A CONSTANT RATE
CALL COLLECT(TC*86400.,CMCONC,ILITE,ITOT)
CALL COLLECT(TE*86400.,EDCONC,ILITE,ITOT)
CALL COLLECT(TD*86400.,DWCONC,ILITE,ITOT)
CALL COLLECT(TM*86400.,CMCONC,ILITE,ITOT)
CALL COLLECT(TN*86400.,EDCONC,ILITE,ITOT)
IF(REGENT.LE.0.0) GO TO 50
CALL STORAG(TRG*86400.,RINV,ILITE,ITOT)
DO 100 I=1,ITOT
50
NZ=NUCL(I)/10000
TURBDR(I)=1991.*5.*SCON(I)
IF(NZ.EQ.1) GO TO 100
IF(NZ.EQ.35.OR.NZ.EQ.53) GO TO 60
IF(NZ.EQ.37.OR.NZ.EQ.55) GO TO 70
CHEMICAL TREATMENT FOR OTHER CATIONS
C
C
C
CWCONC(I)=CWCONC(I)/DFCM
EDCONC(I)=EDCONC(I)/DFED
DWCONC(I)=DWCONC(I)/DFDW
DWCON2(I)=DWCON2(I)/DFD2
CMCONC(I)=CMCONC(I)*(1.0-BDTRF*(1.0-CMFD/DFCM))
C
C
TO TREAT PWR TURBINE BUILDING FLOOR DRAINS THROUGH DIRTY WASTE
SYSTEM, DELETE C FOR COMMENT ON CARDS BELOW, UNTIL NEXT MESSAGE
RINV(I)=RINV(I)/DFRG
TURBDR(I)=1991.*5.*SCON(I)*FPEF/DFDM
461. TURBDR(I)=1991.*5.*SCON(I)*FPEF/DFDM
462. GO TO 100
C
CHEMICAL TREATMENT FOR ANIONS
C
C
C
60
CWCONC(I)=CWCONC(I)/DFICM
EDCONC(I)=EDCONC(I)/DFIED
DWCONC(I)=DWCONC(I)/DFIDW
DWCON2(I)=DWCON2(I)/DFID2
CMCONC(I)=CMCONC(I)*(1.0-BDTRF*(1.0-CMFD/DFICM))
RINV(I)=RINV(I)/DFIRG
TURBDR(I)=1991.*5.*SCON(I)*HEF
473. TURBDR(I)=1991.*5.*SCON(I)*HEF/DFIDW
474. GO TO 100
C
CHEMICAL TREATMENT FOR RB AND CS
C
C
C
70
CWCONC(I)=CWCONC(I)/DFCSCW
EDCONC(I)=EDCONC(I)/DFCSED
DWCONC(I)=DWCONC(I)/DFCSDW
480.

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541. PTOTAL =0.0
542. PPER=0.0
543. PNORM=0.0
544. TLAUND=0.0
545. CTOTAL=0.0
546. PRINT 9001, REACTR
547. PRINT 9006
548. PRINT 9010
549. KOUNTR=1
550. I1=ILITE+IACT+1
551. L=1
552. DO 180 I=1,ITOT
553. IF(I.EQ.I1) PRINT 9011
554. NZ=NUCL(I)/10000
555. IF(NZ.EQ.36.0R.NZ.EQ.54) GO TO 180
556. IF(NZ.EQ.1) GO TO 180
557. DISI=DIS(I)*1.6283E+13
558. APRIM=PCONC(I)*DISI
559. ASEC=0.0
560. CWASTE=CMCONC(I)
561. DWASTE=DWCONC(I)
562. ABLW=CMCONC(I)
563. TB=TURBDR(I)
564. TOTAL=CWASTE+DWASTE+ABLW+TB
565. TOTALN=TOTAL*AOR
566. NUCLI=NUCL(I)
567. XLAUND=0.0
568. TOTALG=TOTALN
569. IF(NUCLI.NE.LAUNDY(L)) GO TO 155
570. XLAUND=WLAUND(L)*PFLAUN
571. TOTALG=TOTALN+WLAUND(L)*PFLAUN
572. L=L+1
573. 155 CONTINUE
574. IF (TOTALG.LT.1E-5) GO TO 156
575. ISUB=2
576. IF (TOTALG.GT.1.) ISUB=1
577. DIV=10.** (INT(ALOG10(TOTALG))-ISUB)
578. TOTALG=AIN(TOTALG/DIV+0.5)*DIV
579. 156 CONTINUE
580. IF(NUCL(I).EQ.10030) TOTALN=TOTAL
581. IF(NZ.EQ.1) GO TO 160
582. SAPRIM=SAPRIM+APRIM
583. SSEC=SSEC+ASEC
584. SABLW=SABLW+ABLW
585. SCWAST=SCWAST+CWASTE
586. SDWAST=SDWAST+DWASTE
587. STB=STB+TB
588. STOTAL=STOTAL+TOTAL
589. SCNORM=SCNORM+TOTALN
590. TLAUND=TLAUND+XLAUND
591. CTOTAL=CTOTAL+TOTALG
592. IF(TOTALG.LT.1E-5) GO TO 180
593. IF(MOD(KOUNTR,50).NE.0) GO TO 170
594. PRINT 9000, REACTR
595. PRINT 9006
596. CALL N0AH(NUCL(I),NAME)
597. THALF=8.0225E-6/DIS(I)
598. PRINT 9007, NAME,THALF,APRIM,CWASTE,DWASTE,
599. 1 ABLW,TOTAL,TOTALN,XLAUND,TOTALG
600. KOUNTR=KOUNTR+1

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601. IF(NZ, EQ, 1) GO TO 180
602. PAPRIM=PAPRIM+APRIM
603. PSEC=PSEC+ASEC
604. PCWAST=PCWAST+CWASTE
605. PDWAST=PDWAST+DWASTE
606. PABLOW=PABLOW+ABLOW
607. PTB=PTB+TB
608. PTOTAL=PTOTAL+TOTAL
609. PNORM=PNORM+TOTALN
610. CONTINUE
611. PAPRIM=SAPRIM-PAPRIM
612. PSEC=SSEC-PSEC
613. PCWAST=SCWAST-PCWAST
614. PDWAST=SDWAST-PDWAST
615. PABLOW=SABLOW-PABLOW
616. PTB=STB-PTB
617. PTOTAL=STOTAL-PTOTAL
618. PNORM=SNORM-PNORM
619. ISUBC=2
620. IF (CTOTAL, GT, 1.) ISUBC=1
621. DIV=10.*(INT(ALOG10(CTOTAL))-ISUBC)
622. CTOTAL=AINT(CTOTAL/DIV+0.5)*DIV
623. IF (PNORM, LT, 1E-5) GO TO 184
624. DIV=10.*(INT(ALOG10(PNORM))-2)
625. PNORM=AINT(PNORM/DIV+0.5)*DIV
626. PNORMT=PNORM
627. PRINT 9008, PAPRIM, PCWAST, PDWAST, PABLOW, PTOTAL, PNORM, PNORMT
628. PRINT 9009, SAPRIM, SCWAST, SDWAST, SABLOW, STOTAL, SCNORM, TLAUND,
629. CTOTAL
630. PRINT 9012, ITRITR
631. 9000 FORMAT(1H1, 20X, 7A4, ' LIQUID EFFLUENTS (CONTINUED)')
632. 9001 FORMAT(1H1, 20X, 7A4, ' LIQUID EFFLUENTS')
633. 9003 FORMAT(1X, A2, I3, A1, 2X, 1PE9.2, 2(2X, E9.2, 2X), 5(1X, 0PF9.5, 1X), 2(1X, 0P
634. 1 F9.5, 1X), 0PF10.5)
635. 9006 FORMAT(1H0, 17X, 'CONCENTRATION ANNUAL RELEASES TO DISCHARGE CAN
636. 1A1, /18X, ' IN PRIMARY ', 43(' '), ' ADJUSTED DETERGENT TOTAL
637. 2 ' /' NUCLEIDE HALF-LIFE COOLANT HIGH PURITY LOW PURITY CHEMICA
638. 3L TOTAL LWS TOTAL WASTES
639. 4I/ML), 3(' (CURIES) '), ' (CURIES) (CI/YR) (CI/Y
640. 5R)')
641. 9007 FORMAT(1X, A2, I3, A1, 2X, 1PE9.2, 2X, E9.2, 2X, 4(1X, 0PF9.5, 1X), 2(1X, 0P
642. 1F9.5, 1X), 1X, 0PF9.5)
643. 9008 FORMAT(1X, 'ALL OTHERS', 9X, 1PE9.2, 2X, 4(1X, 0PF9.5, 1X), 1X, 0PF9.5, 4X,
644. 1 '0.0', 6X, 0PF9.5)
645. 9009 FORMAT(' TOTAL', ' (EXCEPT TRITIUM) ', 1PE9.2, 2X, 4(1X, 0PF9.5, 1X),
646. 1 2(1X, 0PF9.5, 1X), 1X, 0PF9.5)
647. 9010 FORMAT(' CORROSION AND ACTIVATION PRODUCTS')
648. 9011 FORMAT(' FISSION PRODUCTS')
649. 9012 FORMAT(1H0, 1X, 'TRITIUM RELEASE', 12X, I3, ' CURIES PER YEAR')
650. RETURN
651. END
652. BLOCK DATA
653. COMMON /CONB/BCONC(800)
654. DATA BCONC/2*0.0, 0.01, 33*0.0,
655. 1 1E-2, 13*0.0, 2E-4, 53*0.0, 6E-3, 4*0.0, 7E-5, 0.0, 5E-2, 3*0.0,
656. 21E-3, 3*0.0, 3E-5, 0.0, 2E-4, 2*0.0, 4E-4, 7*0.0, 1E-6, 0.0, 3E-4, 2*0.0, 3E-2
657. 3, 4*0.0, 2E-4, 3*0.0, 2E-3, 98*0.0, 3E-4, 64*0.0, 7E-3, 63*0.0, 6E-3, 4*0.0, 7
658. 4E-3, 2*0.0, 3E-3, 19*0.0, 5E-3, 1E-4, 3*0.0, 7E-6, 5*0.0, 4E-3, 0.0, 4E-5, 3*0
659. 5.0, 1E-2, 6E-3, 4*0.0, 4E-3, 11*0.0, 8E-6, 0.0, 8E-6, 6*0.0, 6E-6, 5*0.0, 4E-3
660. 6, 2*0.0, 2E-3, 2E-2, 8*0.0, 9E-2, 7*0.0, 2E-5, 3*0.0, 8E-2, 6*0.0, 2E-3, 4*0.0

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661. 7,3E-6,21*0.,1E-6,104*0.0,4E-5,13*0.,1E-4,0.,3.7E-3,5*0.,1E-5,6E-
662. 82,4*0.0,5E-2,5*0.0,1E-1,2*0.0,3E-5,2*0.0,5E-2,8*0.0,8E-5,3*0.0,2E-
663. 95,4*0.0,1E-2,4*0.0,1E-2,3*0.0,4E-4,4*0.0,1E-2,0.0,3E-5,3*0.0,6E-3,
664. 11E-3,7*0.0,3E-5,4E-5,2*0.0,3E-6,10*0.0,3E-6,81*0.0/
665. END
666. SUBROUTINE SOLVE
667. COMMON/EQ/XZERO(800), XZH(800),XTEMP(800),XNEW(10,800),
668. B(800),D(800)
669. COMMON/FLEX/FLUX(10),MMN,MOUT,INDEX,QXN,AXN,ERR,NOBLND,MZERO
670. COMMON/PROCSS/ MPROS,PRATE(8),NOPROS(8),NZPROS(8,20),PR(800)
671. COMMON/FLUXN/T(20),POWER(10),TOCAP(800),FISS(100),DIS(800),ILITE,
672. IACT,IJFP,ITOT,NON,INPT
673. COMMON/OUT/NUCL(800),TITLE(20),Q(800),FG(800),CUTOFF(7),
674. 1 POW,BURNUP,FLUXB,MSTAR,ALPHAN(100),SPONF(100),ABUND(500),
675. 2 BASIS(10),TCONST,TUNIT
676. DO 10 I=1,ITOT
677. D(I)=-DIS(I)
678. 10 XTEMP(I)=0.0
679. DELT=T(1)*TCONST
680. CALL DECAY(1,DELT,ITOT)
681. CALL TERM(DELT,1,ILITE,ITOT)
682. CALL EQUIL(1,ITOT)
683. DO 30 I=1,ITOT
684. XTEMP(I)=XNEW(I,I)
685. RETURN
686. END
687. SUBROUTINE TERM(T,M,ILITE,ITOT)
688.
689. C
690. C
691. C
692. C
693. C
694. C
695. C
696. C
697. C
698. C
699. C
700. LOGICAL*1 LONG
701. INTEGER*2 LOC,NONO,KD
702. INTEGER*2 LOCP(2500)
703. INTEGER*2 NONP(800)
704. INTEGER*2 NQ,NQU,NQUEUE
705. REAL*8 BATE,BATM
706. REAL*8 CIMN(800),CSUM(800),CIMNI
707. DIMENSION AP(2500),CIMB(800),CIM0(800)
708. DIMENSION QUB(50)
709. COMMON/SERIES/ XP(800),XPAR(800),LONG(800)
710. COMMON/FLEX/FLUX(10),MMN,MOUT,INDEX,QXN,AXN,ERR,NOBLND,MZERO
711. COMMON/EQ/XZERO(800),XZH(800),XTEMP(800),XNEW(10,800),
712. B(800),D(800)
713. COMMON/MATRIX/A(2500),LOC(2500),NON0(800),KD(800)
714. COMMON/DEBUGG/AP
715. COMMON/TERMD/DD(100),DXP(100),QUEUE(50),NQUE(50),NQ(800)
716. NUL=0
717. NN=0
718. C
719. C
720. C
FIRST CONSTRUCT REDUCED TRANSITION MATRIX FOR LONG-LIVED ISOTOPES
DO 220 L=1,ITOT
IF(.NOT.LONG(L)) GO TO 210

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721. NUM=NON0(L)
722. IF(M.GT.MMN.OR.M.EQ.MZERO) NUM=KD(L)
723. CIMP(L)=B(L)
724. IF(NUM.LE.NUL) GO TO 210
725. NS=NN+1
726. N=NUL
727. NL=NUM-NUL
728. DO 200 N1=1,NL
729. N=N+1
730. J=LOC(N)
731. DJ=-D(J)
732.
733.
734.
735.
736.
737.
738.
739.
740.
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743.
744.
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780.

C THIS IS A TEST TO SEE IF ONE OF THE ASYMPTOTIC SOLUTIONS APPLIES
C
C IF(.NOT.LONG(J)) GO TO 10
C NN=NN+1
C AP(NN)=A(N)
C LOGP(NN)=J
C GO TO 200

C GOING BACK UP THE CHAIN TO FIND A PARENT WHICH IS NOT IN
C EQUILIBRIUM
C
C NSAVE=0
C QUE=A(N)/DJ
C DRB=1.0
C CIMP(L)=CIMP(L)+QUE*B(J)
C NQ(L)=0
C NQ(J)=L
C NUX=NON0(J)
C IF(M.GT.MMN.OR.M.EQ.MZERO) NUX=KD(J)
C NUF=0
C IF(J.GT.1) NUF=NON0(J-1)
C NX=NUX-NUF
C IF(NX.LT.1) GO TO 190
C K=NUF
C DO 180 KK=1,NX
C K=K+1
C J1=LOC(K)
C DJ=-D(J1)
C KP=J
C IF(J1.EQ.NQ(KP)) GO TO 180
C KP=NQ(KP)
C IF(KP.NE.0) GO TO 30
C AKDJQ=QUE*(K)/DJ
C IF(.NOT.LONG(J1)) GO TO 160
C TRM=1.0-XP(J1)
C IF(TRM.LT.1.0E-6) GO TO 120
C NQ(J1)=J
C I=1
C KP=J1
C DD(I)=-D(KP)
C DXP(I)=XP(KP)
C KP=NQ(KP)
C IF(KP.EQ.0) GO TO 50
C I=I+1
C IF(I.LE.100) GO TO 40
C IF QUEUE OF SHORT-LIVED NUCLIDES EXCEEDS 100 ISOTOPES, TERMINATE
C CHAIN AND WRITE MESSAGE
C PRINT 9000, M,L,J1,J,AKDJQ
0003600
0003605
0003610
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0003630
0003635
0003640
0003645
0003650
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781. 9000 FORMAT('1100 LONG A QUEUE HAS BEEN FORMED IN TERM',4I5,E12.5)
782. GO TO 190
783. BATE=0.D0
784. IM=I-1
785. DO 110 I=2,IM
786. DL=DD(I)
787. XPL=DXP(I)
788. BATE=0.D0
789. I1=I-1
790. C D R VONDY FORM OF BATEMAN EQUATIONS -- ORNL-TM-361
791. DO 100 KB=1,I1
792. XPJ=DXP(KB)
793. IF(XPJ+XPJ.LT.ERR) GO TO 100
794. DK=DD(KB)
795. PROD=(DL/DK-1.0)
796. DKR=PROD
797. IF(ABS(PROD).GT.1.E-4) GO TO 60
798. USE THIS FORM FOR TWO NEARLY EQUAL HALF-LIVES
799. PROD=TXDK*XPJ*(1.0-0.5*(DL-DJ)*T)
800. GO TO 70
801. PROD=(XPJ-XPL)/PROD
802. PRO1=XPJ/DKR
803. PI=1.0
804. S1=2./(DK*T)
805. DO 90 JK=1,I1
806. IF(JK.EQ.KB) GO TO 90
807. S=1.0-DK/DD(JK)
808. IF(ABS(S).GT.1.E-4) GO TO 80
809. IF(ABS(DKR).GT.1.0E-4) PROD=PRO1
810. S=S1
811. PI=PI*S
812. IF(ABS(PI).GT.1.E25) GO TO 100
813. CONTINUE
814. BATE=BATE+PROD/PI
815. CONTINUE
816. C IF SUMMATION IS NEGATIVE, SET EQUAL TO ZERO AND PRINT MESSAGE
817. IF(BATE.LT.0.D0) PRINT 9001, L,IM,BATE,BATE
818. FORMAT('1BATE IS NEGATIVE IN TERM. THERE ARE MORE THAN TWO SHORT-L
819. LIVED NUCLIDES IN A CHAIN WITH NEARLY EQUAL DIAGONAL ELEMENTS',
820. 2, L,IM,BATE,BATE = ',2I5,1P2E12.5)
821. IF(BATE.LT.0.D0) BATE=0.D0
822. BATE=BATE+BATE
823. CONTINUE
824. DRA=AKDJQ*DJ*(TRM-BATE)/TRM
825. GO TO 130
826. DRA=AKDJQ*AMAX1(DRB,0.0)*DJ
827. IF(NS.GT.NN) GO TO 150
828. DO 140 LJ=NS,NN
829. IF(LOCP(LJ).NE.J1) GO TO 140
830. AP(LJ)=AP(LJ)+DRA
831. GO TO 180
832. CONTINUE
833. NN=NN+1
834. AP(NN)=DRA
835. LOCP(NN)=J1
836. GO TO 180
837. IF(AKDJO.LE.1.0E-06) GO TO 180
838. IF(NSAVE.GE.50) GO TO 180
839. NSAVE=NSAVE+1
840. NQUEUE(NSAVE)=J1
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841.  QUEUE(NSAVE)=AKDJQ
842.  NQU(NSAVE)=J
843.  QUB(NSAVE)=DRB-1./(DJ*NT)
844.  CONTINUE
845.  IF(NSAVE.LE.0) GO TO 200
846.  J=NQUEUE(NSAVE)
847.  QUE=QUEUE(NSAVE)
848.  NQ(J)=NQU(NSAVE)
849.  DRB=QUB(NSAVE)
850.  CIMB(L)=CIMB(L)+QUE*B(J)*AMAX1(DRB,0.0)
851.  NSAVE=NSAVE-1
852.  GO TO 20
853.  CONTINUE
854.  NUL=NONO(L)
855.  NONP(L)=NN
856.  CONTINUE
857.  C FIND NORM OF MATRIX AND ESTIMATE ERROR AS DESCRIBED IN LAPIDUS
858.  C AND LUDS, OPTIMAL CONTROL OF ENGINEERING PROCESSES BLAISDELL 1967
859.  C FIND THE MINIMUM OF THE MAXIMUM ROW SUM AND THE MAXIMUM COLUMN SUM
860.  ASUM=0.0
861.  ASUMJ=0.0
862.  NUL=1
863.  DO 250 I=1,ITOT
864.  IF(.NOT.LONG(I)) GO TO 250
865.  DI=-D(I)*T
866.  AJ=DI
867.  NUM=NONP(I)
868.  IF(NUL.GT.NUM) GO TO 240
869.  DO 230 N=NUL,NUM
870.  AJ=AJ+AP(N)
871.  AI=DI+DI
872.  IF(AI.GT.ASUM) ASUM=AI
873.  IF(AJ.GT.ASUMJ) ASUMJ=AJ
874.  NUL=NONP(I)+1
875.  IF(ASUMJ.LT.ASUM) ASUM=ASUMJ
876.  USE ASUM TO DECIDE HOW MANY TERMS ARE REQUIRED AND ESTIMATE ERROR
877.  NLARGE=3.5*ASUM+.5
878.  XLARGE=NLARGE
879.  ERR1=EXP(ASUM)*(ASUM*.71828/XLARGE)**NLARGE/SQRT(6.2832*XLARGE)
880.  IF(ERR1.GT.1.E-3) PRINT 9002, ERR1,ASUM,NLARGE
881.  9002 FORMAT('0MAXIMUM ERROR GT 0.001, =F10.6,', TRACE='F10.4,
882.  1, NLARGE='I6)
883.  C NEXT GENERATE MATRIX EXPONENTIAL SOLUTION
884.  DO 260 I=1,ITOT
885.  CSUM(I)=XTEMP(I)
886.  CIMN(I)=XTEMP(I)
887.  CONTINUE
888.  ERR3=0.001*ERR
889.  DO 310 NT=1,NLARGE
890.  DO 270 I=1,ITOT
891.  CIMO(I)=CIMN(I)
892.  CONTINUE
893.  TON=T/NT
894.  NUL=1
895.  DO 300 I=1,ITOT
896.  IF(.NOT.LONG(I)) GO TO 300
897.  NUM=NONP(I)
898.  CIMNI=0.0
899.  IF(NT.EQ.1) CIMNI=CIMB(I)
900.  IF(NUL.GT.NUM) GO TO 290

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901. DO 280 N=NUL, NUM
902. J=LOCP(N)
903. CIMNI=CIMNI+AP(N)*CIM0(J)
904. CIMNI=CIMNI+D(I)*CIM0(I)
905. CIMNI=TON*CIMNI
906. IF(DABS(CIMNI).LT.ERR3) CIMNI=0.D0
907. CIMN(I)=CIMNI
908. CSUM(I)=CSUM(I)+CIMNI
909. NUL=NONP(I)+1
910. CONTINUE
911. DO 320 I=1, ITOT
912. IF(CSUM(I).LT.ERR) CSUM(I)=0.0
913. IF(LONG(I)) XNEW(M, I)=CSUM(I)
914. CONTINUE
915. RETURN
916. END
917. SUBROUTINE DECAY(M, T, ITOT)
918. DECAY TREATS SHORT-LIVED ISOTOPES AT BEGINNING OF CHAINS USING
919. BATEMAN EQUATIONS
920. LOGICAL*1 LONG
921. REAL*8 BATE
922. INTEGER*2 LOC, NON0, KD
923. INTEGER*2 NQ, NQU, NQUEUE
924. COMMON/DEBUGG/AP(2500)
925. COMMON/SERIES/ XP(800), XPAR(800), LONG(800)
926. COMMON/FLEX/FLUX(10), MMN, MOUT, INDEX, QXN, AXN, ERR, NOBLND, MZERO
927. COMMON/EQ/XZERO(800), XZH(800), XTEMP(800), XNEW(10, 800),
928. B(800), D(800)
929. COMMON/MATRIX/A(2500), LOC(2500), NON0(800), KD(800)
930. COMMON/TERMD/DD(100), DXP(100), QUEUE(50), NQU(50), NQUEUE(50), NQ(800)
931. DO 10 I=1, ITOT
932. XPAR(I)=0.0
933. LONG(I)=.FALSE.
934. XPI=0.0
935. DT=D(I)*T
936. IF(DT.LT.-50.) GO TO 10
937. IF(ABS(DT).LE.AXN) LONG(I)=.TRUE.
938. XPI=EXP(DT)
939. XP(I)=XPI
940. NUL=1
941. DO 160 L=1, ITOT
942. XTEM=0.0
943. DL=-D(L)
944. NUM=NON0(L)
945. IF(M.GT.MMN.OR.M.EQ.MZERO) NUM=KD(L)
946. IF(NUM.LT.NUL) GO TO 150
947. DO 140 N=NUL, NUM
948. J=LOC(N)
949. DJ=-D(J)
950. IF(LONG(J)) GO TO 140
951. USE THIS FORM FOR TWO NEARLY EQUAL HALF-LIVES
952. IF(ABS(DL/DJ-1.0).LE.1.0E-5) XTEM=XTEM+XTEMP(J)*A(N)*XP(J)*T
953. IF(ABS(DL/DJ-1.0).GT.1.0E-5)
954. 1 XTEM=XTEM+XTEMP(J)*A(N)*(XP(J)-XP(L))/(DL-DJ)
955. QUE=A(N)/DJ
956. NQ(L)=0
957. NQ(J)=L
958. NSAVE=0
959. NUX=NON0(J)
960. IF(M.GT.MMN.OR.M.EQ.MZERO) NUX=KD(L)

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961. NUF=1
962. IF(J.GT.1) NUF=NON0(J-1)+1
963. IF(NUF.GT.NUX) GO TO 130
964. DO 120 K=NUF,NUX
965. J1=L0C(K)
966. IF(LONG(J1)) GO TO 120
967. KP=J
968. IF(J1.EQ.NQ(KP)) GO TO 120
969. KP=NQ(KP)
970. IF(KP.NE.0) GO TO 30
971. DJ=-D(J1)
972. AKDJQ=A(K)/DJ*QUE
973. IF(AKDJQ.LE.1.0E-06) GO TO 120
974. NQ(J1)=J
975. I=1
976. KP=J1
977. DD(I)=-D(KP)
978. DXP(I)=XP(KP)
979. KP=NQ(KP)
980. IF(KP.EQ.0) GO TO 50
981. I=I+1
982. IF(I.LE.100) GO TO 40
983. PRINT 9000, M,L,J1,J,AKDJQ
984. FORMAT('1',4I5,E12.5)
985. GO TO 130
986. BATE=0.D0
987. I1=I-1
988. XPL=XP(L)
989. D R VONDY FORM OF BATEMAN EQUATIONS -- ORNL-TM-361
990. DO 100 KB=1,I1
991. XPJ=DXP(KB)
992. IF(XPL+XPJ.LT.ERR) GO TO 100
993. DK=DD(KB)
994. PROD=(DL/DK-1.0)
995. DKR=PROD
996. IF(ABS(PROD).GT.1.E-4) GO TO 60
997. PROD=T*DK*XPJ*(1.0-0.5*(DL-DJ)*T)
998. GO TO 70
999. PROD=(XPJ-XPL)/PROD
1000. PRO1=XPJ/DKR
1001. PI=1.0
1002. S1=2./(DK*T)
1003. DO 90 JK=1,I1
1004. IF(JK.EQ.KB) GO TO 90
1005. S=1.0-DK/DD(JK)
1006. IF(ABS(S).GT.1.E-4) GO TO 80
1007. USE THIS FORM FOR TWO NEARLY EQUAL HALF-LIVES
1008. IF(ABS(DKR).GT.1.0E-4) PROD=PRO1
1009. S=S1
1010. PI=PI*S
1011. IF(ABS(PI).GT.1.E25) GO TO 100
1012. CONTINUE
1013. BATE=BATE+PROD/PI
1014. CONTINUE
1015. IF(BATE.LT.0.D0) PRINT 9001, L,I,BATE,XTEM,XTEMP(J1),AKDJQ
1016. FORMAT('1',I,BATE,XTEM,XTEMP(J1),AKDJQ = ' ',2I5,1P4E12.5)
1017. IF(BATE.LT.0.D0) BATE=0.D0
1018. XTEM=XTEM+XTEMP(J1)*AKDJQ*BATE
1019. IF(NSAVE.GE.50) GO TO 120
1020. NSAVE=NSAVE+1

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1021. NQUEUE(NSAVE)=J1
1022. QUEUE(NSAVE)=AKDJQ
1023. NQU(NSAVE)=J
1024. CONTINUE
1025. IF(NSAVE.LE.0) GO TO 140
1026. J=NQUEUE(NSAVE)
1027. QUE=QUEUE(NSAVE)
1028. NQ(J)=NQU(NSAVE)
1029. NSAVE=NSAVE-1
1030. GO TO 20
1031. CONTINUE
1032. IF(LONG(L)) XPAR(L)=XTEM/XP(L)
1033. NUL=NONO(L)+1
1034. IF(.NOT.LONG(L)) XNEW(M,L)=XTEM+XTEMP(L)*XP(L)
1035. CONTINUE
1036. DO 170 I=1,ITOT
1037. IF(LONG(I)) XTEMP(I)=XTEMP(I)+XPAR(I)
1038. IF(.NOT.LONG(I)) XTEMP(I)=0.0
1039. CONTINUE
1040. RETURN
1041. END
1042. SUBROUTINE EQUIL(M,ITOT)
1043. C
1044. C EQUIL PUTS SHORT-LIVED DAUGHTERS IN EQUILIBRIUM WITH PARENTS
1045. C EQUIL USES GAUSS-SEIDEL ITERATION TO GENERATE STEADY STATE
1046. C CONCENTRATIONS
1047. C
1048. LOGICAL*1 LONG
1049. INTEGER*2 LOC,NONO,KD
1050. COMMON/EQ/XZERO(800),XZH(800),XTEMP(800),XNEW(10,800),
1051. 1 B(800),D(800)
1052. COMMON/MATRIX/A(2500),LOC(2500),NONO(800),KD(800)
1053. COMMON/FLEX/FLUX(10),MMN,MOUT,INDEX,QXN,AXN,ERR,NOBLND,MZERO
1054. COMMON/SERIES/ XP(800),XPAR(800),LONG(800)
1055. DO 10 I=1,ITOT
1056. XPAR(I)=0.0
1057. IF(.NOT.LONG(I)) GO TO 10
1058. XTEMP(I)=XTEMP(I)*XP(I)
1059. XPAR(I)=AMAX1(XNEW(M,I))-XTEMP(I),0.0)
1060. CONTINUE
1061. ITER=1
1062. N=0
1063. BIG=0.0
1064. DO 60 I=1,ITOT
1065. NUM=NONO(I)-N
1066. DI=-D(I)
1067. IF(LONG(I)) GO TO 50
1068. XNW=B(I)
1069. IF(M.GT.MMN.OR.M.EQ.MZERO) NUM=KD(I)-N
1070. IF(NUM.EQ.0) GO TO 31
1071. DO 30 K=1,NUM
1072. N=N+1
1073. J=LOC(N)
1074. DJ=-D(J)
1075. XJ=XPAR(J)
1076. IF(LONG(J)) XJ=XJ+XTEMP(J)/(1.0-DJ/DI)
1077. XNW=XNW+A(N)*XJ
1078. CONTINUE
1079. C
1080. C 31 XNW=XNW/DI
1080. IF(XNW.LT.1.0E-50) GO TO 40

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1081. ARG=ABS((XNW-XPARG(I))/XNW)
1082. IF(ARG.GT.BIG) BIG=ARG
1083. XPAR(I)=XNW
1084. N=NONO(I)
1085. CONTINUE
1086. IF(BIG.LT.QXN) GOTO 70
1087. ITER=ITER+1
1088. IF(ITER.LT.100) GO TO 20
1089. PRINT 9000
1090. STOP
1091. DO 80 I=1,ITOT
1092. IF(.NOT.LONG(I)) XNEW(M,I)=XNEW(M,I)+XPARG(I)
1093. CONTINUE
1094. RETURN
1095. 9000 FORMAT(' GAUSS SEIDEL ITERATION DID NOT CONVERGE IN EQUIL')
1096. END
1097. SUBROUTINE NUDATA(NLIBE)
1098. NUDATA VERSION TO HANDLE THREE TYPES OF NUCLEAR DATA LIBRARIES
1099. HAS POINTER, NLIBE, = 1 FOR HIGR
1100. C = 2 FOR LIGHT WATER REACTOR
1101. C = 3 FOR LMFBR
1102. C = 4 FOR MSBR
1103. INTEGER*2 LOC, NONO, KD
1104. INTEGER*2 ELE(99), STA(2)
1105. INTEGER*2 KAP(800), MMAX(800)
1106. INTEGER*2 NAME(3)
1107. DIMENSION COEFF(7,800), NPROD(7,800), CAPT(6),
1108. 1 NUCAL(6), NSORS(5), YIELD(5,500), TYLD(5)
1109. DIMENSION Y(5)
1110. DIMENSION SKIP(20)
1111. DIMENSION MSRS(20)
1112. COMMON/LABEL/ELE, STA
1113. COMMON/FLEX/FLUX(10), MMN, MOUT, INDEX, QXN, AXN, ERR, NOBLND, MZERO
1114. COMMON/XEQ/XZERO(800), XZH(800), XTEMP(800), XNEW(10,800),
1115. 1 B(800), D(800)
1116. COMMON/MPC/MPCTAB, AMPC(800), WMPCC(800)
1117. COMMON/FLUXN/T(20), POWER(10), TOCAP(800), FISS(100), DIS(800), ILITE,
1118. 1 IACT, TFP, ITOT, NON, INPT
1119. COMMON/OUT/NUCL(800), TITLE(20), Q(800), FG(800), CUTOFF(7),
1120. 1 POW, BURNUP, FLUXB, MSTAR, ALPHAN(100), SPONF(100), ABUND(500),
1121. 2 BASIS(10), ICONST, TUNIT
1122. COMMON/MATRIX/A(2500), LOC(2500), NONO(800), KD(800)
1123. EQUIVALENCE (XZERO(1), KAP(1)), (XZERO(401), MMAX(1)),
1124. 1 EQUIVALENCE (XZH(1), COEFF(1,1)), (XNEW(1,401), NPROD(1,1))
1125. EQUIVALENCE (A1, DLAM)
1126. DATA NUCAL/-20030, -10000, 10, 11, -10, -9/
1127. DATA MSRS/922330, 922330, 902320, 922380, 942390, 922330, 922350, 942410,
1128. 1 922380, 942390, 942410, 922350, 942400, 922380, 942390, 922330,
1129. 2 922350, 902320, 922380, 942390/
1130. C
1131. C
1132. C
1133. C
1134. C
1135. C
1136. C
1137. C
1138. C
1139. C
1140. C
PROGRAM TO COMPUTE A MATRIX (TRANSITION MATRIX) FROM NUCLEAR DATA
READ 9011, (TITLE(I), I=1, 18), NLIBE
IF(NLIBE.LT.0) PROGRAM WILL READ TAPE IN CASDAR FORMAT
IGWC=0
IF(NLIBE.GT.0) GO TO 10
IGWC=1
NLIBE=-NLIBE
PRINT 9000
9000 FORMAT('H0, 'WILL READ TAPE GENERATED BY CASDAR')

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1141. N1=4-NLIBE
1142. READ 9001, THERM,RES,FAST,ERR,NMO,NDAY,NYR,MPCTAB,INPT,IR
1143. PRINT 9005, NMO,NDAY,NYR
1144. PRINT 9006,
1145. PRINT 9007,
1146. PRINT 9008,
1147. PRINT 9009,
1148. PRINT 9010,
1149. PRINT 9013,
1150. PRINT 9014,
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1196. C
1197. C
1198. C
1199. C
1200. C

THERM,RES,FAST,ERR,NMO,NDAY,NYR,MPCTAB,INPT,IR
NMO,NDAY,NYR

THERM = RATIO OF THERMAL FLUX TO TOTAL FLUX
RES = RATIO OF RESONANCE FLUX TO TOTAL FLUX
FAST = RATIO OF FAST FLUX TO TOTAL FLUX
ERR = TRUNCATION ERROR LIMIT

READ DATA FOR LIGHT ELEMENTS
K=5*(NLIBE-1)
DO 30 K1=1,5
K2=K+K1
NSORS(K1)=MSRS(K2)
PRINT 9018, THERM,RES,FAST,(NSORS(K),K=1,5),NLIBE
I=0
NUTAPE=0
I=I+1
READ(8,9034,END=260)NUCL(I),DLAM,IU,FB1,FP,FP1,FT,FA,FSF,
IF(IGWC.GT.0) GO TO 70
DO 60 N=1,NLIBE
READ(8,9035) SIGTH,FNG1,FNA,FNP,RITH,FINA,FINP,SIGMEV,FN2N1,FFNA,
FFNP,IT
GO TO 90
DO 80 N=1,NLIBE
READ(8,9040) SIGTH,FNG1,FNA,FNP,RITH,FINA,FINP,SIGMEV,FN2N1,FFNA,
FFNP,IT
IF(N1.EQ.0) GO TO 110
DO 100 N=1,N1
READ(8,9036) SKIP
IF(IT.EQ.0) GO TO 50
M=0
CALL HALF(A1,IU)
NUCLI=NUCL(I)
IF(NUCLI.EQ.0) GO TO 260
CALL NOAH(NUCLI,NAME)
IF(MOD(I-1,50).EQ.0) PRINT 9012, (TITLE (N),N=1,18)
IF(MOD(I-1,50).EQ.0) PRINT 9016
SIGTH=THERM*SIGTH
RITH=RES*RITH
SIGMEV=FAST*SIGMEV
SIGNA=SIGTH*FNA+RITH*FINA+SIGMEV*FFNA
SIGNP=SIGTH*FNP+RITH*FINP+SIGMEV*FFNP
FNG=1.0-FNA-FNP
IF(FNG.LT.1.0E-4)FNG=0.
FNG=1.0-FINA-FINP
IF(FING.LT.1.0E-4)FING=0.
FN2N=1.0-FFNA-FFNP
IF(FN2N.LT.1.0E-4)FN2N=0.
SIGNG=SIGTH*FNG+RITH*FING
SIGN2N=SIGMEV*FN2N

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1201. 130 PRINT 9033, NAME, DLAM,FB1,FP,FP1,FT,FA,SIGNG,
1202. FNG1,SIGN2N,FN2N1,SIGNA,SIGNP,Q(I),FG(I),ABUND(I)
1203. C TEST RADIOACTIVITY
1204. C
1205. 140 IF(A1.LE.ERR) GO TO 180
1206. ABETA=1.0
1207. C
1208. C TEST POSITRON EMISSION
1209. C
1210. IF(FP .LT. ERR) GO TO 150
1211. M=M+1
1212. COEFF(M,I)=FP*A1
1213. NPROD(M,I)=NUCLI-10000
1214. ABETA=ABETA-FP
1215. C
1216. C TEST POSITRON EMISSION TO EXCITED STATE OF PRODUCT NUCLIDE
1217. C
1218. IF(FP1 .LT. ERR) GO TO 150
1219. M=M+1
1220. COEFF(M,I)=FP1*COEFF(M-1,I)
1221. NPROD(M,I)=NPROD(M-1,I)+1
1222. COEFF(M-1,I)=COEFF(M-1,I)-COEFF(M,I)
1223. C
1224. C TEST ISOMERIC TRANSITION
1225. C
1226. 150 IF(FT .LT.ERR) GO TO 160
1227. M=M+1
1228. COEFF(M,I)=FT*A1
1229. NPROD(M,I)=NUCLI
1230. ABETA=ABETA-FT
1231. C
1232. C TEST ALPHA EMISSION
1233. C
1234. 160 IF(FA .LT. ERR) GO TO 170
1235. M=M+1
1236. COEFF(M,I)=FA*A1
1237. NPROD(M,I)=NUCLI-20040
1238. M=M+1
1239. COEFF(M,I)=COEFF(M-1,I)
1240. NPROD(M,I)=20040
1241. ABETA=ABETA-FA
1242. C
1243. C TEST NEGATRON EMISSION
1244. C
1245. 170 IF(ABETA.LT.1.E-4) GO TO 180
1246. M=M+1
1247. COEFF(M,I)=ABETA*A1
1248. NPROD(M,I)=NUCLI+10000
1249. C
1250. C TEST NEGATRON EMISSION TO EXCITED STATE OF PRODUCT NUCLIDE
1251. C
1252. IF(FB1 .LT. ERR)GO TO 180
1253. M=M+1
1254. COEFF(M,I)=FB1*COEFF(M-1,I)
1255. NPROD(M,I)=NPROD(M-1,I)+1
1256. COEFF(M-1,I)=COEFF(M-1,I)-COEFF(M,I)
1257. C
1258. C COMPUTE NEUTRON CAPTURE CROSS SECTIONS IN THREE REGIONS
1259. C
1260. 180 KAP(I)=M

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330 IF(MOD(IACT,50).EQ.0) PRINT 9024
PRINT 9026, NAME, DLAM,FB1,FP,FP1,FT,FA,FSF,SIGNG,
1 FNG1,SIGF,SIGN2N,SIGN3N,Q(I),FG(I)
340 IACT=IACT+1
C TEST RADIOACTIVITY
C IF(A1.LT.ERR) GO TO 380
C ABETA=1.0
C TEST POSITRON EMISSION
C IF(FP .LT. ERR) GO TO 350
C ABETA=ABETA-FP
C M=M+1
C COEFF(M,I)=FP*A1
C NPROD(M,I)=NUCLI-10000
C POSITRON EMISSION TO EXCITED STATE
C IF(FP1 .LT. ERR)GO TO 350
C M=M+1
C COEFF(M,I)=FP1*COEFF(M-1,I)
C NPROD(M,I)=NPROD(M-1,I)+1
C COEFF(M-1,I)=COEFF(M-1,I)-COEFF(M,I)
C ISOMERIC TRANSITION
C IF(FT .LT.ERR)GO TO 360
C M=M+1
C COEFF(M,I)=FT*A1
C NPROD(M,I)=NUCLI
C ABETA=ABETA-FT
C ALPHA EMISSION
C IF(FA .LT.ERR)GO TO 370
C M=M+1
C COEFF(M,I)=FA*A1
C NPROD(M,I)=NUCLI-20040
C M=M+1
C COEFF(M,I)=COEFF(M-1,I)
C NPROD(M,I)=20040
C ABETA=ABETA-FA
C BETA DECAY
C IF(ABETA.LT.1.E-4) GO TO 380
C M=M+1
C COEFF(M,I)=ABETA*A1
C NPROD(M,I)=NUCLI+10000
C IF(FB1 .LT. ERR)GO TO 380
C M=M+1
C COEFF(M,I)=COEFF(M-1,I)*FB1
C COEFF(M-1,I)=COEFF(M-1,I)-COEFF(M,I)
C NPROD(M,I)=NPROD(M-1,I)+1
C NEUTRON CAPTURE CROSS SECTIONS
C KAP(I)=M
C DO 390 K=1,6
C CAPT(K )=0.0
C CAPT(2)=SIGNG*FNG1
C CAPT(1)=SIGNG-CAPT(2)
C CAPT(4)=SIGN2N*FN2N1
C CAPT(3)=SIGN2N-CAPT(4)
C FISS(IACT)=SIGF
C TOCAP(I)=0.0
C DO 410 K=1,4
C CAPKI=CAPT(K)
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1381. IF(CAPKI.LT.ERR) GO TO 410
1382. M=M+1
1383. TOCAP(I)=TOCAP(I)+CAPKI
1384. COEFF(M,I)=CAPKI
1385. NPROD(M,I)=NUCLI+NUCAL(K+2)
1386. CONTINUE
1387. TOCAP(I)=TOCAP(I)+FISS(IACT)
1388. N-JN CROSS SECTION
1389. A17=SIGN3N
1390. IF(A17.LT.ERR) GO TO 420
1391. M=M+1
1392. COEFF(M,I)= A17
1393. NPROD(M,I)= NUCLI-20
1394. TOCAP(I)=TOCAP(I)+A17
1395. IF(MOD(NUCLI,10).EQ.0) GO TO 440
1396. DO 430 K=1,M
1397. NPROD(K,I)=NPROD(K,I)-1
1398. MMAX(I)=M
1399. IF(M.GT.7) PRINT 9039, M
1400. SPONF(IACT)=FSF*A1*6.023E23
1401. ALPHAN(IACT)=FA*A1*6.023E13*Q(I)**3.65
1402. DIS(I)=A1
1403. I=I+1
1404. GO TO 270
1405. IL=0
1406. DO 460 K=1,5
1407. TYLD(K)=0.0
1408.
1409. C
1410. C
1411. C
1412. READ DATA FOR FISSION PRODUCTS
1413. READ(8,9034,END=690)NUCL(I),DLAM,IU,FB1,FP,FP1,FT,FA,FSF,
1414. 1Q(I),FG(I),DUMMY,WMP(CI),AMPC(I)
1415. DO 480 N=1,NLIBE
1416. READ(8,9038)SIGNG,RING,FNG1,Y,IT
1417. IF(N1.EQ.0) GO TO 500
1418. DO 490 N=1,N1
1419. READ(8,9036) SKIP
1420. IF(IT.EQ.0) GO TO 470
1421. M=0
1422. CALL HALF(A1,IU)
1423. NUCLI=NUCL(I)
1424. IF(NUCLI.EQ.0) GO TO 690
1425. CALL NOAH(NUCLI,NAME)
1426. IF(MOD(IL,50).EQ.0) PRINT 9012, (TITLE(N),N=1,18)
1427. SIGNG=THERM*SIGNG+RES*RING
1428. IF(NLIBE.EQ.3) GO TO 540
1429. IF(MOD(IL,50).EQ.0) PRINT 9019
1430. PRINT 9021, NAME, DLAM,FB1,FP,FP1,FT,SIGNG,
1431. 1 FNG1,Y,Q(I),FG(I)
1432. GO TO 550
1433. IF(MOD(IL,50).EQ.0) PRINT 9020
1434. PRINT 9022, NAME, DLAM,FB1,FP,FP1,FT,SIGNG,FNG1,
1435. 1 Y(2),Y(4),Y(5),Q(I),FG(I)
1436. C
1437. C
1438. C
1439. TEST RADIOACTIVITY
1440. IF(A1.LT.ERR) GO TO 600
1441. ABETA=1.0
1442. POSITRON EMISSION
1443. A3=FP
1444. C

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1501. MMAX(I)=M
1502. IF(M.GT.7) PRINT 9039, M
1503. DIS(I)=A1
1504. I=I+1
1505. GO TO 470
1506. IFP=IL
1507.
C
1508. ALL DATA ON NUCLIDES HAS BEEN READ, BEGIN TO COMPUTE MATRIX COEFF
1509.
C
1510. ITOT=I-1
1511.
C
1512. FIND PRODUCT NUCLIDES FOR REACTIONS OF LIGHT ELEMENTS
1513.
C
1514. NON=0
1515. DO 700 K=1,ITOT
1516. NON0(K)=0
1517. IF(ILITE.LT.1) GO TO 760
1518. DO 750 I=1,ILITE
1519. NUCL=NUCL(I)
1520. DO 720 J=1,ILITE
1521. KMAX=KAP(J)
1522. IF(KMAX.LT.1) GO TO 720
1523. DO 710 M=1,KMAX
1524. IF(NUCLI.NE.NPROD(M,J)) GO TO 710
1525. NON0(I)=NON0(I)+1
1526. NON=NON+1
1527. IF(NON.GT.2500) PRINT 9041, NON,NUCL(I)
1528. A(NON)=COEFF(M,J)
1529. JT=J
1530. LOC(NON)=JT
1531. CONTINUE
1532. CONTINUE
1533. KD(I)=NON0(I)
1534. DO 740 J=1,ILITE
1535. K1=KAP(J)+1
1536. KMAX=MMAX(J)
1537. IF(KMAX.LT.K1) GO TO 740
1538. DO 730 M=K1,KMAX
1539. IF(NUCLI.NE.NPROD(M,J)) GO TO 730
1540. NON0(I)=NON0(I)+1
1541. NON=NON+1
1542. IF(NON.GT.2500) PRINT 9041, NON,NUCL(I)
1543. A(NON)=COEFF(M,J)
1544. JT=J
1545. LOC(NON)=JT
1546. CONTINUE
1547. CONTINUE
1548. CONTINUE
1549.
C
1550. NON ZERO MATRIX ELEMENTS FOR THE ACTINIDES
1551.
C
1552. IF(IACT.LT.1) GO TO 820
1553. IO=ILITE+1
1554. I1=ILITE+IACT
1555. DO 810 I=IO,I1
1556. NUCL=NUCL(I)
1557. DO 780 J=IO,I1
1558. MAX=KAP(J)
1559. IF(MAX.LT.1) GO TO 780
1560. DO 770 M=1,MAX

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1561. IF(NUCLI.NE.NPROD(M,J)) GO TO 770
1562. NON0(I)=NON0(I)+1
1563. NON=NON+1
1564. IF(NON.GT.2500) PRINT 9041, NON,NUCL(I)
1565. A(NON)=COEFF(M,J)
1566. JT=J
1567. LOC(NON)=JT
1568. CONTINUE
1569. 770 CONTINUE
1570. 780 KD(I)=NON0(I)
1571. DO 800 J=I0,I1
1572. M1=KAP(J)+1
1573. M2=MMAX(J)
1574. IF(M2.LT.M1) GO TO 800
1575. DO 790 M=M1,M2
1576. IF(NUCLI.NE.NPROD(M,J)) GO TO 790
1577. NON0(I)=NON0(I)+1
1578. NON=NON+1
1579. IF(NON.GT.2500) PRINT 9041, NON,NUCL(I)
1580. A(NON)=COEFF(M,J)
1581. JT=J
1582. LOC(NON)=JT
1583. CONTINUE
1584. 790 CONTINUE
1585. 800 CONTINUE
1586. 810 CONTINUE
1587. C
1588. C
1589. 820 MATRIX ELEMENTS FOR FISSION PRODUCTS
1590. IF(IFP.LT.1) GO TO 900
1591. IM=ILITE+IAC
1592. IO=IM+1
1593. IF(IITOT.LI.IO) GO TO 900
1594. DO 880 I=IO,IITOT
1595. NUCL=NUCL(I)
1596. I2=MAX0(IO,I-10)
1597. I3=MIN0(IITOT,I+10)
1598. DO 840 J=I2,I3
1599. KMAX=KAP(J)
1600. IF(KMAX.LT.1) GO TO 840
1601. DO 830 M=1,KMAX
1602. IF(NUCLI.NE.NPROD(M,J)) GO TO 830
1603. NON0(I)=NON0(I)+1
1604. NON=NON+1
1605. IF(NON.GT.2500) PRINT 9041, NON,NUCL(I)
1606. A(NON)=COEFF(M,J)
1607. JT=J
1608. LOC(NON)=JT
1609. CONTINUE
1610. 830 CONTINUE
1611. 840 KD(I)=NON0(I)
1612. DO 860 J=I2,I3
1613. K1=KAP(J)+1
1614. KMAX=MMAX(J)
1615. IF(KMAX.LT.K1) GO TO 860
1616. DO 850 M=K1,KMAX
1617. IF(NUCLI.NE.NPROD(M,J)) GO TO 850
1618. NON0(I)=NON0(I)+1
1619. NON=NON+1
1620. IF(NON.GT.2500) PRINT 9041, NON,NUCL(I)
1620. A(NON)=COEFF(M,J)

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1621. JT=J
1622. LOC(NON)=JT
1623. CONTINUE
1624. CONTINUE
1625. IF(IACT.LT.1) GO TO 880
1626. DO 870 K=1,5
1627. IL=I-IM
1628. IF(YIELD(K,IL).LT.ERR) GO TO 870
1629. NON=NON+1
1630. IF(NON.GT.2500) PRINT 9041, NON, NUCL(I)
1631. NON(I)=NON(I)+1
1632. KK=NSORS(K)
1633. LOC(NON)=KK
1634. KF=KK-ILITE
1635. A(NON)=YIELD(K,IL)*FISS(KF)
1636. CONTINUE
1637. 870
1638. CONTINUE
1639. IF(I.FP.LE.0) GO TO 900
1640. IF(NLIBE.NE.3) GO TO 890
1641. PRINT 9027, TYLD(2), TYLD(4), TYLD(5)
1642. GO TO 900
1643. PRINT 9030, (TYLD(I),I=1,5)
1644. C
1645. C ALL MATRIX ELEMENTS ARE NOW COMPUTED
1646. C BEGIN TRANSIENT SOLUTION
1647. C
1648. C TEMPORARILY WRITE OUT MATRIX ELEMENTS
1649. C
1650. 900 IF(I.R.EQ.0) RETURN
1651. PRINT 9029
1652. N=0
1653. DO 910 I=1,ITOT
1654. NUM=NON(I)
1655. IF(NUM.LE.0) GO TO 910
1656. N1=N+NUM
1657. N=N+1
1658. PRINT 9028, I, DIS (I), TOCAP(I), (A(K), LOC(K), K=N, N1)
1659. N=N1
1660. CONTINUE
1661. RETURN
1662. 920 STOP
1663. C
1664. C FORMATS FORMATS FORMATS FORMATS
1665. C
1666. 9001 FORMAT(4F10.5,6I2)
1667. 9002 FORMAT(I6,F5.3,I1,5F3.3,E5.2,F3.3,
1668. F4.3,F3.3,F6.4)
1669. 9003 FORMAT(I6,F5.3,I1,3X,4F3.3,2E5.2,F3.3,5E5.2,F4.3,F3.3)
1670. 9004 FORMAT(I6,F5.3,I1,5F3.3,2E5.2,F3.3,4E5.2,F3.3,F4.3,F3.3,2E5.2)
1671. 9005 FORMAT(1H1,43X,'NUCLEAR TRANSMUTATION DATA REVISIED',I2,'',I2,'
1672. 1',I2,'',ORUCL = NUCLEIDE = 10000 * ATOMIC NO + 10 * MASS NO + ISOM
1673. 2ERIC STATE (0 OR 1)',10X,'DLAM = DECAY CONSTANT (1/SEC)',/,',', FB,
1674. 3JEP, FA, FT = FRACTIONAL TRANSITION. FB = 1 - FP - FA - FT',/,',', FB1,
1675. 4REP, ALPHA, INTERNAL TRANSITION. FB = 1 - FP - FA - FT',/,',', FB1,
1676. 5 FP1, FNG1, FN2N1 = FRACTION OF BETA, POSITRON, N-GAMMA, N-2N TRAN
1677. 6SITIONS TO EXCITED STATE OF PRODUCT NUCLIDE',/,',', SIGTH, SIGNG, SIG
1678. 7F, SIGNA, SIGNP = THERMAL CROSS SECTIONS (BARNS) FOR ABSORPTION, N
1679. 8-GAMMA, FISSION, N-ALPHA, N-PROTON.',)
1680. 9006 FORMAT(' SIGNG = SIGHT * (1 - FNA -FNP). SIGNA = SIGHT * FNA.

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1681. SIGNP = SIGTH * FNP. FNA, FNP = FRACTION THERMAL N-ALPHA, N-PROTON 0008400
 1682. 2N, RITH, RING, RINF, RINA, RINP = RESONANCE INTEGRAL FOR ABSOR 0008405
 1683. 3PTION, N-GAMMA, FISSON, N-ALPHA, N-PROTON, RING = RITH * (0008410
 1684. 41 - FINA - FINP). RINA = RITH * FINA. RINP = RITH * FINP. FINA, F 0008415
 1685. 5INP = FRACTION RESONANCE N-ALPHA, N-PROTON, RITH * SIGMEV, SIGFF, SI 0008420
 1686. 6GN2N, SIGNAF, SIGNPF = FAST CROSS SECTIONS (BARNS) FOR ABSORPTION, 0008425
 1687. 7FISSION, N-2N, N-ALPHA, N-PROTON, SIGN2N = SIGMEV * (1 - FF 0008430
 1688. 8NA - FFNP). SIGNAF = SIGMEV * FENA. SIGNPF = SIGMEV * FFNP. FFN 0008435
 1689. 9A, FFNP = FRACTION FAST N-ALPHA, N-P. 0008440
 9007 FORMAT(Y23, Y25, Y28, Y28, Y49 = FISSON YIELD (PERCENT) FROM 23 0008445
 15-U, 235-U, 232-TH, 238-U, 239-PU, Q = HEAT PER DISINTEGRATI 0008450
 20N. FG = FRACTION OF HEAT IN GAMMAS OF ENERGY GREATER THAN 0.2 ME 0008455
 3V, EFFECTIVE CROSS SECTIONS FOR A VOLUME AVERAGED THERMAL (L 0008460
 4T 0.876 EV) FLUX ARE AS FOLLOWS. N-GAMMA - SIGNG * THERM 0008465
 5 + RING * RES. FISSON - SIGF * THERM + RIF * RES + SIGF 0008470
 6F * FAST. 10X, THERM = 1/V CORRECTION FOR THERMAL SPECTRUM AND TE 0008475
 7PERATURE. N-2N - SIGN2N * FAST. 36X, RES = RATIO 0008480
 80F RESONANCE FLUX PER LETHARGY UNIT TO THERMAL FLUX. 0008485
 9008 FORMAT(N-ALPHA - SIGNA * THERM + RINA * RES + SIGNAF * FAST 0008490
 1, 7X, FAST = 1.45 * RATIO OF FAST (GT 1.0 MEV) TO THERMAL FLUX 0008495
 2, N-PROTON - SIGNP * THERM + RINP * RES + SIGNPF * FAST. 0008500
 1 THERMAL POWER, C M LEDERER, J M HOLLANDER, AND I PERLMAN, TAB 0008505
 2 ILE OF ISOTOPES - SIXTH EDITION, JOHN WILEY AND SONS, INC (1967), 0008510
 3, B S DZHELEPOV AND L K PEKER, DECAY SCHEMES OF RADIOACTIVE NUC 0008515
 4 LEI, PERGAMON PRESS (1961), D T GOLDMAN AND JAMES R ROSSER, 0008520
 5 CHART OF THE NUCLIDES, NINTH EDITION, GENERAL ELECTRIC CO (JULY 0008525
 6 1966), E D ARNOLD, PROGRAM SPECTRA, APPENDIX A OF ORNL-3576 0008530
 7 (APRIL 1964)) 0008535
 9010 FORMAT(CROSS SECTIONS AND FLUX SPECTRA, B E PRINCE, NEUT 0008540
 IRON REACTION RATES IN THE MSRE SPECTRUM, ORNL-4119, PP 79-83 (JUL 0008545
 2Y 1967), B E PRINCE, NEUTRON ENERGY SPECTRA IN MSRE AND MSBR, 0008550
 3, ORNL-4191, PP 50-58 (DEC 1967), M D GOLDBERG ET AL, NEUTRON 0008555
 4 CROSS SECTIONS, BNL-325, SECOND ED, SUPP NO 2 (MAY 1964 - AUG 19 0008560
 566) (ALSO EARLIER EDITIONS), H T KERR, UNPUBLISHED ERC COMPILATI 0008565
 6 ON (FEB 1968), M K DRAKE, A COMPILATION OF RESONANCE INTEGRAL 0008570
 75, NUCLEONICS, VOL 24, NO 8, PP 108-111 (AUG 1966), BNWL STAF 0008575
 8F, INVESTIGATION OF N-2N CROSS SECTIONS, BNWC-98, PP 44-98 (JUNE 0008580
 9 1965)) 0008585
 9011 FORMAT(184, I3) 0008590
 9012 FORMAT(1H1, 20X, 18A4) 0008595
 9013 DURING REACTOR IRRADIATION, H ALTER AND C E WEBER, PRODUCTION OF H AND HE IN METALS 0008600
 2, L BENNETT, RECOMMENDED FISSION PRODUCT CHAINS FOR USE IN 0008605
 3 REACTOR EVALUATION STUDIES, ORNL-TM-1658 (SEPT 1966)) 0008610
 9014 FORMAT(FISSON PRODUCT YIELDS, M E MEEK AND B F RIDER, 0008620
 1 SUMMARY OF FISSION PRODUCT YIELDS FOR U-235, U-238, PU-239, AND PU 0008625
 2-241 AT THERMAL, FISSION SPECTRUM AND, 14 MEV NEUTRON ENERGI 0008630
 3ES, APED-5398-(REV.), (OCT. 1968), S KATCOFF, FISSION PRODUCT 0008635
 4 YIELDS FROM NEUTRON INDUCED FISSION, NUCLEONICS, VOL 18, NO 11, 0008640
 5 (NOV 1960), N D DUDEY, REVIEW OF LOW-MASS ATOM PRODUCTION IN F 0008645
 6 AST REACTORS, ANL-7434, (APRIL 1968)) 0008650
 9015 FORMAT(1H0, 20X, LIGHT ELEMENTS, MATERIALS OF CONSTRUCTION, AND ACT 0008655
 1 IVATION PRODUCTS, 10 NUCL DLAM FB1 FP FPI FT 0008660
 2A SIGHT FNG1 FNA FNP RITH FINA FINP SIGMEV FN2N1 0008665
 3 FFNA FFNP Q FG) 0008670
 9016 FORMAT(1H0, 20X, LIGHT ELEMENTS, MATERIALS OF CONSTRUCTION, AND ACT 0008675
 1 IVATION PRODUCTS, 10 NUCL DLAM FB1 FP FPI FT 0008680
 2A SIGNG FNG1 SIGN2N FN2N1 SIGNA SIGNP Q FG ABU 0008685
 3NDANCE)) 0008690
 1740. 0008695

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9017 FORMAT(1H ,A2,I3,A1,1PE9.2,0P5F6.3,1PE9.2,0P3F6.3,1PE9.2,0P2F6.3,
11PE9.2,0P4F6.3,0PF5.2)
9018 FORMAT(1H0,10X ,THERM= 'F10.5,5X,RES= 'F10.5,5X,'FAST= 'F10.5,
1/,1X,'NEUTRON SOURCE= '5(I10,5X),5X,'NLIBE= 'I3)
9019 FORMAT(1H0,36X,'FISSION PRODUCTS',/,0 NUCL
1 FP1 FT SIGNG ' , FNG1 Y23 Y25 Y02 Y02 Y
228 Y49 Q , FG')
9020 FORMAT(1H0,36X,'FISSION PRODUCTS',/,0 NUCL DLAM FB1 FP
1 FP1 FT SIGNG FNG1 Y25 Y28 Y49 Q FG')
9021 FORMAT(1H ,A2,I3,A1,1PE9.2,0P4F6.3,1PE9.2,0PF6.3,1P5E9.2,
10P2F6.3)
9022 FORMAT(1H ,A2,I3,A1,1PE9.2,0P4F6.3,1PE9.2,0PF6.3,1P3E9.2,0P2F6.3)
9023 FORMAT(1H0,32X, 'ACTINIDES AND THEIR DAUGHTERS',/,
1, NUCL DLAM FB1 FP FT FA FSF E+6 SIGNG R
2ING FNG1 SIGF RIF RIF 'SIGFF SIGN2N SIGN3N Q FG')
9024 FORMAT(1H0,32X, 'ACTINIDES AND THEIR DAUGHTERS',/,
1, NUCL DLAM FB1 FP FT FA FSF E+6 SIGNG F
2NG21 SIGF SIGN2N SIGN3N Q FG')
9025 FORMAT(1H ,A2,I3,A1,1PE9.2,0P5F6.3,6PF6.1,1P2E9.2,0PF6.3,1P5E9.2,
1 OPF6.3,F5.2)
9026 FORMAT(1H ,A2,I3,A1,1PE9.2,0P5F6.3,6PF9.1,1PE9.2,0PF6.3,1P3E9.2,
1 OPF7.3,F5.2)
9027 FORMAT('OSUM OF YIELDS OF ALL FISSION PRODUCTS =',15X,1P3E9.2)
9028 FORMAT(15,2X,1PE10.3,3X,E10.3,5(2X,E10.3,3X,I5)/(30X,5(2X,E10.3,
3X,I5)))
9029 FORMAT('NON-ZERO MATRIX ELEMENTS AND THEIR LOCATIONS',/
1, I DIS(I) J CAP(I) A(I,J) J A(I,J) J '
2J A(I,J) A(I,J) A(I,J) A(I,J)
9030 FORMAT(64HOSUM OF YIELDS OF ALL FISSION PRODUCTS
1,1P5E9.2)
9031 FORMAT(5I110)
9032 FORMAT(16,F5.3,I1,5F3.3,E5.2,3F3.3,E5.2,2F3.3,E5.2,3F3.3,F4.3,F3.3
1,F6.4)
9033 FORMAT(1H ,A2,I3,A1,1PE9.2,0P5F6.3,1PE9.2,0PF6.3,1PE9.2,0PF6.3,
1P2E9.2,0P2F6.3,F7.3)
9034 FORMAT(17,F9.3,I1,5F5.3,1PE9.2,0P2F5.3,F7.3,2E6.0)
9035 FORMAT(7X,F9.2,3F5.3,F9.2,2F5.3,F9.2,3F5.3,5X,I1)
9036 FORMAT(20A4)
9037 FORMAT(7X,2F9.2,F5.3,4F9.2,F4.3,F9.2,I1)
9038 FORMAT(7X,2F9.2,F5.3,5F9.2,4X,I1)
9039 FORMAT('0 WARNING, MOUT OF RANGE IN NUDATA, = ' I5)
9040 FORMAT( 7X,F9.2,3F8.6,F4.2,2F3.1,F9.2,3F5.3,5X,I1)
9041 FORMAT('0 NON HAS EXCEEDED 2500, EQUAL TO '2I6)
END
SUBROUTINE COLECT(TMB,CWASTE,ILITE,ITOT)
COMMON/EO,XZERO(800), XZH(800),XTEMP(800),XNEW(10,800),
1 B(800),D(800)
DIMENSION CWASTE(800)
IF(TMB.LT.1) RETURN
DO 10 I=1,ITOT
B(I)=CWASTE(I)
XTEMP(I)=0.0
CALL DECAY(1,TMB,ITOT)
CALL TERM(TMB,1,0,ITOT)
CALL EQUIL(1,ITOT)
DO 20 I=1,ITOT
CWASTE(I)=XNEW(1,I)/TMB
RETURN
END
SUBROUTINE STORAG(TMB,CWASTE,ILITE,ITOT)

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1801. COMMON/EQ/XZERO(800), XZH(800), XTEMP(800), XNEW(10,800),
1802. B(800), D(800)
1803. DIMENSION CWASTE(ITOT)
1804. IE(TMB.LT.1) RETURN
1805. DELT=TMB
1806. DO 10 I=1, ITOT
1807. B(I)=0.0
1808. XTEMP(I)=CWASTE(I)
1809. CALL DECAY(I, DELT, ITOT)
1810. CALL TERM(TMB, I, ILITE, ITOT)
1811. CALL EQUIL(I, ITOT)
1812. DO 20 I=1, ITOT
1813. CWASTE(I)=XNEW(I, I)
1814. RETURN
1815. END
1816. PROGRAM BLOCK DATA
1817. BLOCK DATA
1818. INTEGER*2 ELE(99), STA(2)
1819. COMMON/LABEL/ ELE, STA
1820. DATA ELE/ 'H', 'HE', 'LI', 'BE', 'B', 'C', 'N', 'O', 'F', 'NE', 'NA', 'M
1821. 'G', 'AL', 'SI', 'P', 'S', 'CL', 'AR', 'K', 'CA', 'SC', 'TI', 'V', 'CR', 'MN
1822. 'FE', 'CO', 'NI', 'CU', 'Zn', 'GA', 'GE', 'AS', 'SE', 'BR', 'KR', 'RB', 'SR'
1823. 'Y', 'ZR', 'NB', 'MO', 'TC', 'RU', 'RH', 'PD', 'AG', 'CD', 'IN', 'SN', 'SB',
1824. 'TE', 'I', 'Xe', 'CS', 'BA', 'LA', 'CE', 'PR', 'ND', 'PM', 'SM', 'EU', 'GD',
1825. 'DY', 'HO', 'ER', 'TM', 'YB', 'LU', 'HF', 'TA', 'W', 'RE', 'OS', 'IR', 'P
1826. 'AU', 'HG', 'TL', 'PB', 'BI', 'PO', 'AT', 'RN', 'FR', 'RA', 'AC', 'TH', 'PA
1827. 'U', 'NP', 'PU', 'AM', 'CM', 'BK', 'CF', 'ES'
1828. DATA STA/ 'M', '
1829. END
1830. SUBROUTINE HALF(A, I)
1831. SUBROUTINE HALF CONVERTS HALF-LIFE TO DECAY CONSTANT (1/SEC)
1832. DIMENSION C(9)
1833. DATA C/6.9315E-01, 1.1552E-02, 1.9254E-04, 8.0226E-06, 2.1965E-08, 0.0,
1834. 2.1965E-11, 2.1965E-14, 2.1965E-17/
1835. IF(A.GT.0.0) GO TO 10
1836. IF(I.EQ.6) GO TO 20
1837. A=9.99
1838. RETURN
1839. A=C(I)/A
1840. RETURN
1841. A=0.0
1842. RETURN
1843. END
1844. SUBROUTINE NOAH(NUCLI, NAME)
1845. SUBROUTINE NOAH CONVERTS SIX DIGIT IDENTIFIER TO ALPHAMERIC SYMBOL
1846. INTEGER*2 NAME(3)
1847. COMMON/LABEL/ ELE, STA
1848. IS=MOD(NUCLI, 10)+1
1849. NZ =NUCLI/10000
1850. MJ=NUCLI/10-NZ *1000
1851. NAME(1)=ELE(HZ)
1852. NAME(2)=MJ
1853. NAME(3)=STA(IS)
1854. RETURN
1855. END
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61. C DECONI DEFINES THE DECAY CONSTANT FOR IODINES 0000300
62. C 0000305
63. C DATA DECONI/9.970E-07,9.170E-06/ 0000310
64. C 0000315
65. C CBWR DEFINES THE REACTOR WATER CONCENTRATIONS FOR IODINES 0000320
66. C 0000325
67. C 0000330
68. C DATA CBWR/3.7E-3,5.0E-2/ 0000335
69. C 0000340
70. C RN DEFINES THE NORMALIZED ANNUAL RELEASES DURING POWER OPERATIONS FOR 0000345
71. C THE REACTOR BLDG. 0000350
72. C 0000355
73. C 0000360
74. C DATA RN/12.3,12.3/ 0000365
75. C 0000370
76. C RNS DEFINES THE NORMALIZED ANNUAL RELEASES DURING SHUTDOWNS FOR THE 0000375
77. C REACTOR BLDG. 0000380
78. C 0000385
79. C DATA RNS/5.2,5.2/ 0000390
80. C 0000395
81. C RNT DEFINES THE NORMALIZED ANNUAL RELEASES DURING POWER OPERATION FOR 0000400
82. C THE TURBINE BLDG. 0000405
83. C 0000410
84. C DATA RNT/3.8E3,3.8E3/ 0000415
85. C 0000420
86. C RNTS DEFINES THE NORMALIZED ANNUAL RELEASES DURING SHUTDOWNS FOR 0000425
87. C THE TURBINE BLDG. 0000430
88. C 0000435
89. C DATA RNTS/4.1E2,4.1E2/ 0000440
90. C 0000445
91. C RNR DEFINES THE NORMALIZED RELEASES FROM THE RADWASTE BLDG. DURING 0000450
92. C POWER OPERATIONS 0000455
93. C 0000460
94. C DATA RNR/4.6,4.6/ 0000465
95. C 0000470
96. C RNRS DEFINES THE NORMALIZED RELEASES FROM THE RADWASTE BLDG. 0000475
97. C DURING SHUTDOWNS 0000480
98. C 0000485
99. C DATA RNRS/1.4,1.4/ 0000490
100. C 0000495
101. C RMVP DEFINES NORMALIZED RELEASES FROM THE MECHANICAL VACUUM PUMP 0000500
102. C DATA RMVP/4.9E2,4.9E2/ 0000505
103. C DATA RNMP/1.1E3,1.1E3/ 0000510
104. C 49 FORMAT(16X,'REACTOR VESSEL HALOGEN CARRYOVER FACTOR',15X,F10.5) 0000515
105. C 51 FORMAT(16X,'PLANT CAPACITY FACTOR',T74,'0.80') 0000520
106. C 52 FORMAT(32X,8A4,12X,A4) 0000525
107. C 53 FORMAT(16X,13A4,A2,F10.5) 0000530
108. C 55 FORMAT(15X,4A4,A2,8X,F8.0,7X,F5.3) 0000535
109. C 56 FORMAT(20X,F8.0,2(5X,F8.0)) 0000540
110. C 57 FORMAT(27X,F6.2,14X,F6.2,18X,F6.2) 0000545
111. C 58 FORMAT (30X,'FRACTION FRACTION COLLECTION DECAY',/8X,'STREAM 1
FLOW RATE OF PCA DISCHARGED TIME',5X,' DECONTAM (DAYS)',7X,
21NATION FACTORS',/20X,',(GAL/DAY)',23X, '(DAYS)
3'I',8X,'CS',8X,'OTHERS')
59 FORMAT(2X,4A4,A2,1PE9.2,1X,4(OPF8.3,2X),3(1PE9.2,1X))
60 FORMAT(79X,I1)
61 FORMAT(16X,'THERE IS A CRYOGENIC DISTILLATION COLUMN',/20X,' IODINE
AND XENON DECONTAMINATION FACTOR',T70,'10000.',/20X,'KRYPTON DECONT
AMINATION FACTOR',T71,'4000.',/20X,'KRYPTON AND XENON HOLDUP TIME
3(DAYS)',T73,'90.')

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121. 62 FORMAT(16X, 'THERE IS NO CHARCOAL DELAY SYSTEM')
 122. 63 FORMAT(16X, 'THERE IS A CHARCOAL DELAY SYSTEM', /20X, 'KRYPTON HOLDUP
 123. 1 TIME (DAYS)', T72, F9.5/20X, 'XENON HOLDUP TIME (DAYS)', T72, F9.5/
 124. 220X, 'KRYPTON DYNAMIC ADSORPTION COEFFICIENT (CM3/GM)', T72, F9.5/
 125. 320X, 'XENON DYNAMIC ADSORPTION COEFFICIENT (CM3/GM)', T71, F10.5/20X,
 126. 4'MASS OF CHARCOAL (THOUSAND LBS)', T72, F9.5)
 127. 68 FORMAT(70X, F10.5)
 128. 77 FORMAT(16X, 'FRACTION IODINE BYPASSING CONDENSATE DEMINERALIZER',
 129. 17X, T72, F9.5)
 130. 71 FORMAT(2X, 'REGENERANT SOLS ', 1PE9.2, 14X, 0PF5.3, 2X, 2(F8.3, 2X),
 131. 13(1PE9.2, 1X))
 132. 903 FORMAT(16X, 16A4)
 133. 904 FORMAT (/, ' LIQUID WASTE INPUTS')
 134. 905 FORMAT (/, ' GASEOUS WASTE INPUTS')
 135. 906 FORMAT(1H)
 136. 907 FORMAT('0', 15X, 'THERE IS NOT AN ON-SITE LAUNDRY')
 137. 214 FORMAT(1H, 131H)
 138. -----
 139. 2-----
 140. 232 FORMAT(1H0, 5X, 'TOTAL NOBLE GASES', 99X, 1PE7.1)
 141. 230 FORMAT(1H0, 4X, A8, 5X, 1PE9.3, 8X, 1PE7.1, 1X, 6(4X, 1PE7.1, 1X), 7X, 1PE7.1)
 142. 231 FORMAT(1H0, '0.0 APPEARING IN THE TABLE INDICATES RELEASE IS LESS
 143. 1 THAN 1.0 CI/YR FOR NOBLE GAS')
 144. 245 FORMAT(1H0, 49X, 'AIRBORNE PARTICULATE RELEASE RATE', /1H0, 63X, '(CURI
 145. 1ES PER YEAR)', /1H0, 32X, 'CONTAINMENT', 3X, 'TURBINE', 6X, 'AUXILIARY', 4X
 146. 2, 'RADWASTE MECH VAC', /1H, 4X, 'NUCLIDE', 24X, 'BLDG.', 7X, 'BLDG.', 7X,
 147. 3'BLDG.', 8X, 'BLDG.', 6X, 'PUMP', 10X, 'TOTAL')
 148. 235 FORMAT(1H0, 63X, 'GASEOUS RELEASE RATE', /1H0, 63X, '(CURIES PER YEAR)', /
 149. 11H0, 16X, 'COOLANT CONC', 3X, 'CONTAINMENT', 3X, 'TURBINE', 4X, 'AUXILIAR
 150. 2Y', 3X, 'RADWASTE', 5X, 'GLAND', 7X, 'AIR', 6X, 'MECH VAC', /1H, 4X, 'NUCLIDE',
 151. 3, 3X, '(MICROCURIES/G)', 6X, 'BLDG.', 7X, 'BLDG.', 7X, 'BLDG.', 6X, 'BLDG.',
 152. 48X, 'SEAL', 5X, 'EJECTOR', 7X, 'PUMP', 11X, 'TOTAL')
 153. 925 FORMAT(16X, 4A4, 10X, F4.0, 6X, F4.0)
 154. 927 FORMAT(16X, 4A4, 10X, F4.0, 6X, F4.0)
 155. 926 FORMAT(16X, 4A4, 'IODINE RELEASE FRACTION', 16X, F10.5/32X, 'PARTICULA
 156. 1TE RELEASE FRACTION', 10X, F10.5)
 157. 928 FORMAT(16X, 4A4, 'IODINE RELEASE FRACTION', 16X, F10.5/32X, 'PARTICULAT
 158. 1E RELEASE FRACTION', 10X, F10.5)
 159. 920 FORMAT(1H0, 4X, A8, 22X, 5(1PE7.1, 5X), 3X, 1PE7.1)
 160. 960 FORMAT(1H0, 30X, 'H-3 RELEASED FROM TURBINE BLDG. VENTILATION SYSTEM
 161. 1, 5X, 1PE7.1)
 162. 962 FORMAT(1H0, 30X, 'H-3 RELEASED FROM CONTAINMENT BLDG. VENTILATION SY
 163. 1STEM', 5X, 1PE7.1)
 164. 963 FORMAT(1H0, 30X, 'C-14 RELEASED VIA MAIN CONDENSER OFFGAS SYSTEM =
 165. 19.5 CI/YR')
 166. 964 FORMAT(1H0, 30X, 'TOTAL H-3 RELEASED VIA GASEOUS PATHWAY', 5X, 1PE7.1)
 167. 2 FORMAT(I2)
 168. C
 169. C
 170. C
 171. C
 172. C
 173. C
 174. C
 175. C
 176. C
 177. C
 178. C
 179. C
 180. C

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GENERIC PLANT INFORMATION
 READ(1, 2) N
 ICOUNT = 0
 IFCOUNT = ICOUNT + 1
 IFCOUNT.EQ.N) GO TO 1003
 READ(1, 52) NAME, TYPE
 WRITE(6, 906)
 WRITE(6, 52) NAME, TYPE
 READ(1, 53) WORD, POWTH
 WRITE(6, 53) WORD, POWTH
 OPFRA=0.80

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181. WRITE(6,51)
182. READ(1,53)WORD,GTO
183. WRITE(6,53)WORD,GTO
184. READ(1,53)WORD,WLIQ
185. WRITE(6,53)WORD,WLIQ
186. READ(1,53)WORD,GDE
187. WRITE(6,53)WORD,GDE
188. PC = 0.015
189. READ(1,53)WORD,REGENT
190. IF(REGENT.EQ.0.0) PC = 0.004
191. WRITE(6,53)WORD,REGENT
192. READ(1,53)WORD,FFCDM
193. WRITE(6,53)WORD,FFCDM
194. WRITE(6,49) PC
195.
196.
197.
198.
199.
200.
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202.
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238.
239.
240.
WRITE(6,904)
READ(1,55)WARD,CWFLR,CWA
READ(1,56)DFICW,DFCSCM,DFCW
READ(1,57)TC,TSTORC,CWFD
WRITE(6,58)
READ(1,55)WARD,CWFLR,CWA,CWFD,TC,TSTORC,DFICW,DFCSCM,DFCW
READ(1,56)DFIDW,DFCSDM,DFDW
READ(1,57)TD,TSTORD,DWFD
WRITE(6,59)WARD,DWFLR,DWA,DWFD,TD,TSTORD,DFIDW,DFCSDM,DFDW
READ(1,55)WARD,DFICM,DFCSCM,DFCM
READ(1,57)TCM,TSTORB,CWFD
WRITE(6,59)WARD,CWFLR,CWA,CWFD,TCM,TSTORB,DFICM,DFCSCM,DFCM
READ(1,68)RGWFR
READ(1,56)DFIRG,DFCSRG,DFRG
READ(1,57)TRG,TSTORR,RGFD
WRITE(6,71)RGWFR,RGFD,TRG,TSTORR,DFIRG,DFCSRG,DFRG
READ DATA FOR BWR GAS CODE
WRITE(6,905)
READ(1,53)WORD,GGG
WRITE(6,53)WORD,GGG
READ(1,53)WORD,TIM3
WRITE(6,53)WORD,TIM3
READ(1,53)WORD,TIM4
WRITE(6,53)WORD,TIM4
HEPA1=1.0
FIL1=1.0
HEPA2=1.0
FIL2=1.0
HEPA5=1.0
FIL5=1.0
HEPA6=1.0
FIL6=1.0
FILGS = 1.0
FILEJ = 1.0
READ(1,925)WURD,CBCH,CBHEPA
IF(CBCH.GT.0.0)FIL1 = (1.0 - CBCH/100.)
IF(CBHEPA.GT.0.0)HEPA1 = (1.0 - CBHEPA/100.)
WRITE(6,926)WURD,FIL1,HEPA1
READ(1,927)WURD,TBCH,TBHEPA

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C
C
C

C
C
C

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241. IF(TBCH.GT.0.0)FIL2 = (1.0 - TBCH/100.)
242. IF(TBHEPA.GT.0.0)HEPA2 = (1.0 - TBHEPA/100.)
243. WRITE(6,928) WURD,FIL2,HEPA2
244. READ(1,53) WORD,FIL3
245. IF(FIL3.GT.0.0) FILGS = (1.0 - FIL3/100.)
246. WRITE(6,53) WORD,FILGS
247. READ(1,53) WORD,FIL4
248. IF(FIL4.EQ.1.0) FILEJ = (1.0 - FIL4)
249. IF(FIL4.GT.1.0) FILEJ = (1.0 - FIL4/100.)
250. IF(FIL4.EQ.0.0) FILEJ = 1.0
251. WRITE(6,53) WORD,FILEJ
252. READ(1,925) WURD,AXCH,AXHEPA
253. IF(AXCH.GT.0.0)FIL5 = (1.0 - AXCH/100.)
254. IF(AXHEPA.GT.0.0)HEPA5 = (1.0 - AXHEPA/100.)
255. WRITE(6,926) WURD,FIL5,HEPA5
256. READ(1,925) WURD,RWCH,RWHEPA
257. IF(RWCH.GT.0.0)FIL6 = (1.0 - RWCH/100.)
258. IF(RWHEPA.GT.0.0)HEPA6 = (1.0 - RWHEPA/100.)
259. WRITE(6,926) WURD,FIL6,HEPA6
260. READ(1,60)KCHAR
261. READ(1,53)WORD,KKR
262. READ(1,53)WORD,KXE
263. READ(1,53)WORD,KMASS
264. IF(KXE.LT.1161.) XKAR = 6.4
265. IF(KXE.GT.1161.) XKAR = 16.0
266. IF(KCHAR.EQ.0) GO TO 90
267. IF(KCHAR.EQ.1) GO TO 91
268. WRITE(6,61)
269. CHT11=90.
270. CHT12=90.
271. CHT3=90.
272. GO TO 92
273. 90 WRITE(6,62)
274. CHT11=0.
275. CHT12=0.
276. CHT3=0.
277. GO TO 92
278. 91 CHT11 = 1.8 * (KMASS * KKR)/POWTH
279. CHT12 = 1.8 * (KMASS * KXE)/POWTH
280. CHT3 = 1.8 * (KMASS * XKAR)/POWTH
281. WRITE(6,63)CHT11,CHT12,KKR,KXE,KMASS
282. CONTINUE
283. READ(1,53) WORD,PFLAUN
284. IF(PFLAUN.LE.0.0) WRITE(6,907)
285.
286. C
287. C
288. C
289. C
290. C
291. C
292. C
293. C
294. C
295. C
296. C
297. C
298. C
299. C
300. C
CONVERSION OF UNITS
GTO=GTO*1000000.
GDE=GDE*1000000.
GGS=GGS*1000.
WLIQ=WLIQ*1000000.
WSTE=WSTE*1000000.
TOT=1
IF(FFCDM.LT.0.99) FFCDM = 0.18
IF(ABS(POWTH-3400).GT.400.1) GO TO 210
IF(ABS(WLIQ-3.8E5).GT.0.4001E5)GO TO 210
IF(ABS(GDE-1.3E5).GT.0.2001E5)GO TO 210
IF(ABS(GTO-1.5E7).GT.0.2001E7)GO TO 210
IF(FFCDM.GT.0.99) GO TO 210
0001200
0001205
0001210
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0001220
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0001250
0001255
0001260
0001265
0001270
0001275
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301. GO TO 211
302. 210 RHAL2=(GDE*0.9+FFCDM*GTO*PC*0.9)/WLIQ
303. IOT=2
304. 211 CONTINUE
305.
306. C
307. C CALCULATION OF IODINE RELEASES FROM BLDG. VENTILATION SYSTEMS
308. C
309. C DO 88 I = 1,2
310. CBWR1(I) = CBWR(I)
311. DECOHI(I) = DECOHI(I) * 3600.
312. EX3(I) = DECOHI(I) * TIM3
313. IF(EX3(I).GT.75.) EX3(I) = 75.
314. EX4(I) = DECOHI(I) * TIM4
315. IF(EX4(I).GT.75.) EX4(I) = 75.
316. IF(IOT.EQ.1) GO TO 2002
317. CBWR(I) =CBWR1(I) * ((111.76 * POWTH/WLIQ) * ((0.4038+ DECOHI(I))/C
318. 1RHAL2 + DECOHI(I)))
319.
320. C CALCULATION OF IODINE RELEASES FROM RX. BLDG. DURING NORMAL OPERATIONS
321. C
322. C 2002 CONTINUE
323. RBWR(I) = RN(I) * CBWR(I)
324. AUXBLH(I) = RBWR(I) * 0.9
325. CBLN(I) = RBWR(I) * 0.1
326.
327. C CALCULATION OF IODINE RELEASES FROM RX. BLDG. DURING SHUTDOWNS
328. C
329. RBWRS(I) = RNS(I) * CBWR(I)
330. AUXBLS(I) = RBWRS(I) * 0.1
331. CBL(S(I) = RBWRS(I) * 0.9
332. CBLI(I) = (CBLN(I) + CBL(S(I) * FIL1
333. AUXLI(I) = (AUXBLN(I) + AUXBLS(I)) * FIL5
334.
335. C CALCULATION OF IODINE RELEASES FROM TURBINE BLDG.DURING OPERATION
336. C
337. RBWRT(I) = RNT(I) * CBWR(I) * PC
338. RBWRTS(I) = RNTS(I) * CBWR(I) * PC
339. TBLI(I) = (RBWRT(I) + RBWRTS(I)) * FIL2
340.
341. C
342. RBWRR(I) = RNR(I) * CBWR(I)
343. RBWRRS(I) = RNR(S(I) * CBWR(I)
344. RADBLI(I) = (RBWRR(I) + RBWRRS(I)) * FIL6
345.
346. C
347. IF(GGS.EQ.0.0) GO TO 87
348. SGLI(1) = 8.1E-1 * CBWR(1) * FILGS
349. SGLI(2) = 2.2E-1 * CBWR(2)* FILGS
350. GO TO 99
351. 87 SGLI(1) = 0.0
352. SGLI(2) = 0.0
353.
354. C
355. 99 EXCI(I) = 0.0
356. IF(KCHAR.EQ.2) EXCI(I) = DECOHI(I) * CHTI1 * 24.
357. IF(EXCI(I).GT.75.) EXCI(I) = 75.
358. IF(KCHAR.EQ.2) DFCR = 0.00010
359. EJTI(1) = 6.0 * EXP(-EX4(I))*DFCR+EXP(-EXCI(I))*FILEJ
360. EJTI(2) = EJTI(1) * CBWR(2)/CBWR(1)
361. RMVP(I) = (RNMVP(I) * CBWR(I) * PC) * 4.0
362. IF(I.EQ.2) GO TO 899
363. RNMVPS(I) = RNMVPS(I) * CBWR(I) * PC

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361. RMVPS(2) = RMVP(I) * CBWR(I) * PC
362. VPRI(I) = RMVP(I) + RMVPS(I)
363. TEST = 0.0001
364. IF(SGLI(I).LE.TEST) SGLI(I) = 0.0
365. IF(EJTI(I).LE.TEST) EJTI(I) = 0.0
366. CONTINUE
88 MSIG = 1
   NSIG = 2
   CALL SIGF2(SGLI)
   CALL SIGF2(EJTI)
   DO 89 I = 1,2
371. TOTI(I) = AUXLI(I)+TBLI(I)+SGLI(I)+EJTI(I)+CBLI(I)+RADBLI(I)+VPRI(
372. I)
373. CONTINUE
374. WRITE(6,906)
375. WRITE(6,903) NAME
376. WRITE(6,214)
377. WRITE(6,235)
378. WRITE(6,214)
379. DO 79 I = 1,2
380. WRITE(6,230) HAL(I),CBWR(I),CBLI(I),TBLI(I),AUXLI(I),RADBLI(I),SGL
381. I(I),EJTI(I),VPRI(I),TOTI(I)
382. CBWR(I) = CBWR1(I)
383. CONTINUE
79 WRITE(6,214)
384.
385.
386.
387.
388.
389.
390.
391.
392.
393.
394.
395.
396.
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419.
420.
899 RMVPS(2) = RMVP(I) * CBWR(I) * PC
   VPRI(I) = RMVP(I) + RMVPS(I)
   TEST = 0.0001
   IF(SGLI(I).LE.TEST) SGLI(I) = 0.0
   IF(EJTI(I).LE.TEST) EJTI(I) = 0.0
88 CONTINUE
   MSIG = 1
   NSIG = 2
   CALL SIGF2(SGLI)
   CALL SIGF2(EJTI)
   DO 89 I = 1,2
371. TOTI(I) = AUXLI(I)+TBLI(I)+SGLI(I)+EJTI(I)+CBLI(I)+RADBLI(I)+VPRI(
372. I)
373. CONTINUE
374. WRITE(6,906)
375. WRITE(6,903) NAME
376. WRITE(6,214)
377. WRITE(6,235)
378. WRITE(6,214)
379. DO 79 I = 1,2
380. WRITE(6,230) HAL(I),CBWR(I),CBLI(I),TBLI(I),AUXLI(I),RADBLI(I),SGL
381. I(I),EJTI(I),VPRI(I),TOTI(I)
382. CBWR(I) = CBWR1(I)
383. CONTINUE
79 WRITE(6,214)
384.
385.
386.
387.
388.
389.
390.
391.
392.
393.
394.
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419.
420.
C CALCULATION OF TRITIUM RELEASES
C
C TRITRP = 0.03 * POWTH
  GASH3 = TRITRP * 0.5
  TBH3 = GASH3 * 0.5
  CBH3 = GASH3 - TBH3
  TH3 = TBH3 + CBH3
  DIV = 10.*(INT(ALOG10(TBH3))-1)
  TBH = INT(TBH3/DIV+0.5)*DIV
  DIV = 10.*(INT(ALOG10(CBH3))-1)
  CBH = INT(CBH3/DIV+0.5)*DIV
  DIV = 10.*(INT(ALOG10(TH3))-1)
  TH = INT(TH3/DIV+1.0)*DIV
  WRITE(6,960) TBH
  WRITE(6,962) CBH
  WRITE(6,964) TH
  WRITE(6,963)
C CALCULATION OF NOBLE GAS RELEASES
C
C
  WRITE(6,906)
  WRITE(6,903) NAME
  WRITE(6,214)
  WRITE(6,235)
  WRITE(6,214)
  DO 5 I = 1,14
412. DECOH(I)=DECON(I)*3600.
413. EX3(I)=DECOH(I)*TIM3
414. IF(EX3(I).GT.75.)EX3(I)=75.
415. EX4(I)=DECOH(I)*TIM4
416. IF(EX4(I).GT.75.)EX4(I)=75.
417. X1(I)=XB(I)
418. CBL(I)=CBB(I)
419. AXBL(I)=AXBB(I)
420.

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421. TBL(I)=TBB(I)
422. RADBL(I)=RAD5B(I)
423. SGL(I)=GG5*X1(I)*EXP(-EX3(I))*3.977*OPFRA
424. IF(I.GT.1) GO TO 98
425. EXC(I) = DECOH(I) * CHT3 * 24.
426. GO TO 101
427.
428. 98 EXC(I)=DECOH(I)*CHII1*24.
429. IF(I.GT.7)EXC(I)=DECOH(I)*CHTI2*24.
430. CONTINUE
431. IF(EXC(I).GT.75.)EXC(I)=75.
432. DFCR=0.0
433. IF(KCHAR.EQ.2) DFCR=0.00025
434. IF(LCHAR.EQ.2.AND.I.GT.7) DFCR=0.0001
435. IF(I.GT.1) GO TO 105
436. EJT(I) = 1E3 * EXP(-EX4(I)) * (DFCR + EXP(-EXC(I)))
437. GO TO 2001
438. 105 EJT(I)=GTO*X1(I)*EXP(-EX4(I))*(DFCR+EXP(-EXC(I)))*3.977*OPFRA
439. GO TO 2001
440. 2001 TEST=1.
441. IF(SGL(I).LE.TEST) SGL(I)=0.0
442. IF(EJT(I).LE.TEST) EJT(I)=0.0
443. 5 CONTINUE
444. DO 2003 I=1,14
445. TOT(I)=AXB(I)+TBL(I)+SGL(I)+EJT(I)+CBL(I)+RADBL(I)+VPR(I)
446. 2003 CONTINUE
447. MSIG = 2
448. NSIG = 14
449. CALL SIGF2(TBL)
450. CALL SIGF2(SGL)
451. CALL SIGF2(EJT)
452. GASTOT=0.0
453. DO 2004 I=1,14
454. WRITE(6,230)NUCLID(I),XB(I),CBL(I),TBL(I),AXB(I),RADBL(I),
1 SGL(I),EJT(I),VPR(I),TOT(I)
455. 2004 GASTOT=GASTOT+TOT(I)
456. CONTINUE
457. DIV=10.**((INT(ALOG10(GASTOT))-1)
458. GASTOT=AINI(GASTOT/DIV+0.5)*DIV
459. WRITE(6,232) GASTOT
460. WRITE(6,214)
461. WRITE(6,231)
462. WRITE(6,906)
463. WRITE(6,903)NAME
464. WRITE(6,214)
465. WRITE(6,245)
466. WRITE(6,214)
467. DO 9 I = 1,19
468. PCBL(I) = FCBB(I)*1E-3*HEPA1
469. PTBL(I) = PTBB(I)*1E-3*HEPA2
470. PAXBL(I) = PAXBB(I)*1E-3*HEPA5
471. PVPL(I) = PVPR(I) * 1E-3
472. PRWBL(I) = PRWBB(I)*1E-3*HEPA6
473. PTOTB(I) = PCBL(I) + PTBL(I) + PAXBL(I) + PRWBL(I) + PVPL(I)
474. 9 CONTINUE
475. MSIG = 3
476. NSIG = 20
477. CALL SIGF2(PTOTB)
478. DO 10 I =1,19
479. WRITE (6,920) BPART(I),PCBL(I),PTBL(I),PAXBL(I),PRWBL(I),PVPL(I),
1PTOTB(I)
480.

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481. 10 CONTINUE
482.   WRITE(6,214)
483.   GO TO 80
484. 1003 CONTINUE
485.   STOP
486.   END
487.   SUBROUTINE SIGF2(RLPT)
488.   COMMON MSIG,NSIG
489.   DIMENSION RLPT(NSIG)
490.   IF(MSIG.EQ.2) GO TO 25
491.   IF(MSIG.EQ.3) GO TO 30
492.   DO 20 I=1,NSIG
493.     C THIS PART OF SUBROUTINE IS FOR IODINE
494.     ISUB=2
495.     IF(RLPT(I).EQ.0.) GO TO 20
496.     IF(RLPT(I).GT.1.0)ISUB=1
497.     DIV=10.**INT(ALOG10(RLPT(I)))-ISUB)
498.     RLPT(I)=AINT(RLPT(I)/DIV+0.5)*DIV
499.   20 CONTINUE
500.   GO TO 50
501.   25 CONTINUE
502.   DO 35 I = 1,NSIG
503.     C THIS PART OF SUBROUTINE IS FOR NOBLE GASES
504.     IF(RLPT(I).EQ.0.) GO TO 35
505.     DIV=10.**INT(ALOG10(RLPT(I)))-1)
506.     IF (RLPT(I).LT.10.) DIV=1.00
507.     RLPT(I)=AINT(RLPT(I)/DIV+0.5)*DIV
508.   35 CONTINUE
509.   GO TO 50
510.   30 CONTINUE
511.   DO 40 I = 1,NSIG
512.     C THIS PART OF SUBROUTINE IS FOR PARTICULATES
513.     IF (RLPT(I).EQ.0.) GO TO 40
514.     DIV=10.**INT(ALOG10(RLPT(I)))-2)
515.     RLPT(I)=AINT(RLPT(I)/DIV+0.5)*DIV
516.   40 CONTINUE
517.   50 RETURN
518.   END
519.
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CHAPTER 4. DATA NEEDED FOR NRC RADIOACTIVE SOURCE TERM
CALCULATIONS FOR BOILING WATER REACTORS (BWRs)

This chapter lists the information needed to generate source terms for BWRs. The information is provided by the applicant and should be consistent with the contents of the Safety Analysis Report (SAR) and the Environmental Report (ER) of the proposed boiling water reactor. This information is the basic data required to calculate the releases of radioactive material in liquid and gaseous effluents (the source terms). All data is on a per-reactor basis.

4.1 GENERAL

1. The maximum core thermal power (Mwt) evaluated for safety considerations in the SAR. (Note: All of the following responses should be adjusted to this power level.)
2. The quantity of tritium released in liquid and gaseous effluents (Ci/yr per reactor).

4.2 NUCLEAR STEAM SUPPLY SYSTEM

1. Total steam flow rate (in lb/hr).
2. Mass of reactor coolant (in lb) in the reactor vessel at full power.

4.3 REACTOR COOLANT CLEANUP SYSTEM

1. Average flow rate (in lbs/hr).
2. Demineralizer type (deep bed or powdered resin) and size of resin capacity (in ft³).
3. Regeneration or replacement frequency.
4. Regenerant volume (in gal/event) and activity (if applicable).

4.4 CONDENSATE DEMINERALIZERS

1. Average flow rate (in lbs/hr).
2. Demineralizer type (deep bed or powdered resin).
3. Number and size (in ft³) of resin capacity of demineralizers.
4. Regeneration or replacement frequency.
5. Indicate whether ultrasonic resin cleaning is used and waste liquid volume associated with its use.
6. Regenerant volume (in gal/event) and activity.

4.5 LIQUID WASTE PROCESSING SYSTEMS

1. For each liquid waste processing system, provide in tabular form the following information:
 - a. Sources, flow rates (in gal/day), and expected activities (fraction of primary coolant activity, i.e., PCA) for all inputs to each system.
 - b. Holdup times associated with collection, processing, and discharge of all liquid streams.
 - c. Capacities of all tanks (in gal) and processing equipment (in gal/day) considered in calculating holdup times.
 - d. Decontamination factors for each processing step.

- e. Fraction of each processing stream expected to be discharged over the life of the plant.
 - f. For waste demineralizer regeneration, the time between regenerations, regenerant volumes and activities, treatment of regenerants, and fractions of regenerant discharged. Include parameters used in making these determinations.
 - g. Liquid source term by radionuclide (in Ci/yr) for normal operation, including anticipated operational occurrences.
2. Provide piping and instrumentation diagrams and process flow diagrams for the liquid radwaste systems, along with all other systems influencing the source term calculations.

4.6 MAIN CONDENSER AND TURBINE GLAND SEAL AIR REMOVAL SYSTEMS

1. The main condenser tubing material of construction, i.e., stainless steel or copper.
2. The holdup time (in hr) for offgases from the main condenser air ejector prior to processing by the offgas treatment system.
3. A description and the expected performance of the gaseous waste treatment systems for the offgases from the condenser air ejector and mechanical vacuum pump. The iodine source term from the condenser.
4. The mass of charcoal (in tons) in the charcoal delay system used to treat the offgases from the main condenser air ejector, the operating and dew point temperatures of the delay system, and the dynamic adsorption coefficients for Xe and Kr.
5. A description of the cryogenic distillation system, the fraction of gases partitioned during distillation, the holdup in the system, storage following distillation, and the expected system leakage rate.
6. The steam flow (in lbs/hr) to the turbine gland seal and the source of the steam (primary or auxiliary).
7. The design holdup time (in hr) for gas vented from the gland seal condenser, the iodine partition factor for the condenser, and the fraction of radioiodine released through the system vent. A description of the treatment system used to reduce radioiodine and particulate releases from the gland seal system.
8. Piping and instrumentation diagrams and process flow diagrams for the gaseous waste treatment system, along with all other systems influencing the source term calculations.

4.7 VENTILATION AND EXHAUST SYSTEMS

For each plant building housing the main condenser evacuation system, the turbine gland seal system exhaust, or any system that contains radioactive materials, provide the following:

1. Provisions incorporated to reduce radioactivity releases through the ventilation or exhaust systems.
2. Decontamination factors assumed and the bases (include charcoal adsorbers, HEPA filters, and mechanical devices).
3. Release rates for radioiodines, noble gases, and radioactive particulates (in Ci/yr); and the bases.
4. Release point description including height above grade, height above and location relative to adjacent structures, expected average temperature difference between gaseous effluents and ambient air, flow rate, exit velocity, and size and shape of flow orifice, whether deflectors or diffusers are used.
5. For the containment building, indicate the expected purge and venting frequencies and duration and the continuous purge rate (if used).

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APPENDIX A

LIQUID SOURCE TERM CALCULATIONAL PROCEDURE FOR REGENERANT WASTES FROM DEMINERALIZERS OTHER THAN CONDENSATE DEMINERALIZERS

Often in BWR radwaste systems, demineralizers other than the condensate demineralizers may undergo regeneration, for example, the radwaste demineralizer in the high purity waste system. The BWR-GALE Code can calculate the liquid effluent resulting from periodic regeneration of non-condensate demineralizers by following the procedure outlined below.

1. Input to Cards 1-7 and Cards 17-33

A separate computer run for calculating the regeneration waste effluent from non-condensate demineralizers is required. Cards 1-7 should be filled out as indicated for the specific plant in Sections 1.5.2.1 through 1.5.2.7 of this report. Also Cards 17 through 33 may be left blank. (except that values of 1.0 must be entered for Card 18 entries).

2. Input to Cards 8-16

The only liquid source term data cards completed (Cards 8-16) should be the three card sets used in the input data for the stream in which the demineralizer to be regenerated is located.

a. Input Flow and Activity (Cards 8, 11, or 14)

The input flow rate and input activity should be the average daily input flow rate and input activity processed through the demineralizer to be regenerated. For example, if the demineralizer to be regenerated is used to process a BWR high purity stream, the total input flow rate and weighted activity would be 30,000 gallons per day at 0.15 PCA from Table 1-4.

Note that it is not the flow rate and activity which is due to the regenerant wastes which is entered, it is the normal flow rate and activity through the component to be regenerated which is entered.

b. Regeneration Frequency (Card 9, 12, or 15)

Enter the time between regenerations in days as the "collection time." If a regeneration frequency is stated by the applicant, it may be used; otherwise the following frequency may be used:

TABLE A-1

<u>Demineralizer Service</u>	<u>Regeneration Frequency</u>
Reactor Coolant Cleanup System	180 days
Equipment Drain Wastes	25,000 gal/ft ³ *
Floor Drain Wastes	2,000 gal/ft ³ *

* Calculated values based on 12,000 gm CaCO₃ ion exchange capacity per ft³ of resin and 5 umho/cm and 50 umho/cm average conductivity of equipment and floor drain liquid wastes.

By inputting the normal flow rate and activity in Item a and the regeneration frequency as the collection time in Item b the BWR-GALE Code will accumulate all of the activity processed through the demineralizer during its normal operation and decay the activity as a function of the time over which it was collected.

c. Process Time and Fraction Discharged

Use the same "process time" and "fraction discharged" as indicated for the stream in which the regeneration wastes are processed as indicated in Section 1.5.2.8.2 of this document.

d. Decontamination Factors (Card 10, 13 or 16)

The decontamination factors entered should consider radionuclide removal by the equipment used to process the regenerant wastes using the normal source term procedures of 1.5.2.8.2. In addition, the decontamination factors entered should be used to adjust the source term for the fraction of the activity in the process stream flowing through the demineralizer during normal operation which was not removed by the demineralizer.

e. Sample Case

A waste demineralizer is used to process equipment drain waste and is to be regenerated. The normal flow rate and activity for the demineralizer is 30,000 gpd at 0.15 PCA. The demineralizer resin volume is 180 ft³. The regenerant wastes will be processed through an evaporator and discharged.

Fill in the Cards 8-10 in the following manner:

Card 8

Spaces 18-41 enter - waste demin regen
Spaces 42-49 enter - 30,000
Spaces 57-61 enter - 0.15

Card 9

The wastes will be processed through an evaporator which will provide the following DF's according to Table 1-5 of Section 1.5.2.8.2:

I - 10³
Cs, Rb - 10⁴
Others - 10⁴

While in operation, referring to Table 1-5 of Section 1.5.2.8.2, demineralizer DF's were:

I - 10²
Cs, Rb - 2
Others - 10²

Therefore, for "I" and "Others," 99% of the activity processed through the demineralizer was removed by the resins and no adjustment is needed. Only 50% of the Cs and Rb in the waste stream was removed by the resins, however, so the DF entered for Cs should be adjusted. Thus, the DFs entered on Card 9 would be:

I - 10³
Cs, Rb - 2 × 10⁴
Others - 10⁴

Card 10

Spaces 29-32 "Collection Time." Using the value from Table A-1 of 25,000 gal/ft³, the regeneration frequency would be:

$$\frac{(180 \text{ ft}^3)(25,000 \text{ gal/ft}^3)}{(30,000 \text{ gal/day})} = 150 \text{ days}$$

Enter 150 days in spaces 29-32.

Use the same "process time" and "fraction discharged" as is indicated for the stream in which the regeneration wastes are processed as indicated in Section 1.5.2.8.2 of this report.

3. Components in Service

- a. If the waste is processed through a component other than a regenerable demineralizer prior to processing by the regenerable demineralizer, the activity in the steam entering the demineralizer will be less than the activity entered as described above. To compensate for this difference, the DF's for the regenerant waste calculation should be adjusted in a manner similar to that described above. The product of the DF's should be used.
- b. If two regenerable demineralizers are used in series, follow the procedure in A above. Adjust the DF for nuclides removed from the waste stream, by using the product of the DF's for two demineralizer in series, i.e., consider the two demineralizers as one larger demineralizer.

4. Use of Computer Calculated Result

Combine the values printed out in the individual liquid source term columns for the system in which the demineralizer is being regenerated (not the adjusted total value) with the normal liquid source term run values. Do not use the adjusted total value from the right hand column as the source term run to which the regenerant waste run will be added has already been adjusted.

NRC FORM 335 (7-77)		U.S. NUCLEAR REGULATORY COMMISSION BIBLIOGRAPHIC DATA SHEET		1. REPORT NUMBER <i>(Assigned by DDC)</i> NUREG-0016, Rev. 1	
4. TITLE AND SUBTITLE <i>(Add Volume No., if appropriate)</i> Calculation of Releases of Radioactive Materials in Gaseous and Liquid Effluents from Boiling Water Reactors (BWR-GALE Code)		2. <i>(Leave blank)</i>		3. RECIPIENT'S ACCESSION NO.	
7. AUTHOR(S) Frank P. Cardile and others		5. DATE REPORT COMPLETED MONTH YEAR December 1978		6. <i>(Leave blank)</i>	
9. PERFORMING ORGANIZATION NAME AND MAILING ADDRESS <i>(Include Zip Code)</i> U.S. Nuclear Regulatory Commission Office of Nuclear Reactor Regulation Effluent Treatment Systems Branch Washington, DC 20555		DATE REPORT ISSUED MONTH YEAR January 1979		8. <i>(Leave blank)</i>	
12. SPONSORING ORGANIZATION NAME AND MAILING ADDRESS <i>(Include Zip Code)</i> Same as 9		10. PROJECT/TASK/WORK UNIT NO.		11. CONTRACT NO.	
13. TYPE OF REPORT		PERIOD COVERED <i>(Inclusive dates)</i>			
15. SUPPLEMENTARY NOTES		14. <i>(Leave blank)</i>			
16. ABSTRACT <i>(200 words or less)</i> <p>In April of 1976, the NRC published NUREG-0016. That document presented methods for calculation of releases from BWRs based on operating data available at that time. In promulgating Appendix I to 10 CFR Part 50, the Commission indicated its desire to use the best available data for improving the calculational models. Therefore, at this time, we are updating NUREG-0016 by issuing Revision 1 which incorporates more recent operating data now available and also incorporates the results of a number of in-plant measurement programs at operating BWRs.</p> <p>NUREG-0016, Revision 1, is similar to NUREG-0016 in that it provides instructions for using the BWR-GALE Code. It describes the parameters incorporated in the Code, the input data required, and a step-by-step procedure for completing the input data cards. It provides parameters for an assessment of reactor and radwaste system performance for normal operation including anticipated operational occurrences, and the bases for selecting the parameters. It also contains a Fortran IV listing of the BWR-GALE Code, a form for entering the input data, and a sample calculation.</p>					
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