

Scientific Notebook No. 430: Simulation of
Water Chemistry, Continues in Scientific
Notebook No. 572, (09/20/2000 through
04/07/2006)

CENTER FOR NUCLEAR WASTE REGULATORY ANALYSES

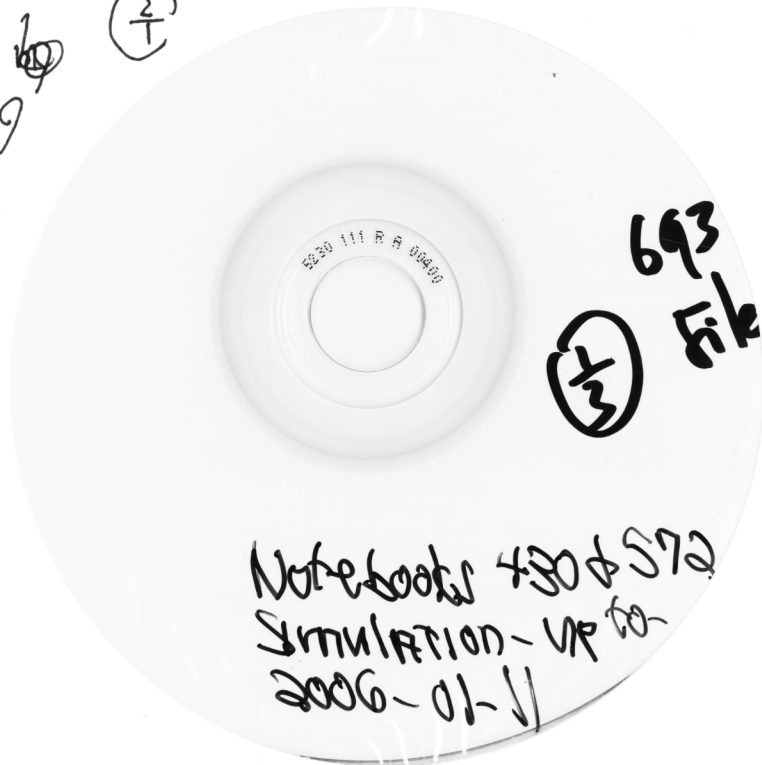
Book # 430
J 13 Water
Simulation.
Evaporation

CNWRA
CONTROLLED
COPY 430

693
File

(1/3)

11-10-9002 of dn 225-057



693
File
(1/3)

Notebooks 430 & 572
Simulation - up to
2006-01-11

Initial Entry.

09/20/00

1

Project # W-1402-561

Sub-project Title: Simulation of waters

* Objective: Simulation of J-13 Water Chemistry During Evaporation.

* Approach: Using OLI Environmental System Program (Esp). V. 6.2d.

Litkai Yang

J-y

J-y

4.1.6.2 Groundwater Chemistry

See Table 18, Major Ion Concentrations for J-13 Well Water.

10⁻⁵ Pa.

Table 19. Average Composition of Synthetic J-13 Water Used in Reported Tests

Species	Synthetic J-13 Water (mg/L)	Average J-13 Water (mg/L)
Ca	6.4	12
Cl ⁻	6.9	6.7
F ⁻	2.2	4.4
HCO ₃ ⁻	108	139
K	5.3	4.7
Mg	2.2	1.9
Na	46	46
NO ₃ ⁻	8.0	8.8
SO ₄ ²⁻	18.1	17
Si(aq)	11.3	57.3
pH	7.84	6.8-8.3

DTN: LL991008104241.042 and LL980711104242.054

NOTE: Average J-13 water composition from Table 18.

All electronic files are stored in: Litkai Yang 09/16/02
NoteBooks/Notebook#430 J.Y.S.
& 577 - simulation 11/17/03

09/20/00

Table 20. Average Composition of SPW Used in Reported Tests

Ions	Synthetic Porewater (mg/L)	Average Porewater (mg/L) ^A
Ca ²⁺	57.3 ± 1.80	101
Cl ⁻	76.6 ± 1.30	117
F ⁻	2.16 ± 0.09	0.86
HCO ₃ ⁻	20.3 ± 4.30	200 ^B
K ⁺	4.0 ± 0.27	8.0
Mg ²⁺	11.8 ± 0.20	17
Na ⁺	8.56 ± 0.32	61.3
NO ₃ ⁻	10.7 ± 0.29	Note C
SO ₄ ²⁻	83.9 ± 1.90	116
SiO ₂ (aq)	22.2 ± 2.1	70.6
pH	7.55 ± 0.12	8.32 (25°C)

DTN: LL991008004241.041 and LB991200DSTTHC.001 (TBV-4575)

- NOTES: A Averages from porewater samples ESF-HD-PERM1(30.1'-30.5').
 B Total dissolved inorganic carbon reported as bicarbonate; calculated from charge balance.
 C Not analyzed.

Table 16. The Compositions of Evaporatively Concentrated Simulated 100x Well J-13 Water.

Species	Starting Solution (mg/L)	Solution Compositions (mg/L) and the Estimated Boiling Point (°C)							
		Sample #	ECBP 042399-0	ECBP 050699-0	ECBP 051899-0	ECBP 060199-0	ECBP 061099-0	ECBP 061499-0	ECBP 061599-0
Boiling Point (°C)			101					108	
Ca	6	735	0	0	48	0	62	587	
K	535	3885	7985	15878	21180	24510	21532	8389	
Mg	0	0	0	0	0	0	0	0	
Na	4360	43317	106465	177301	202726	226721	190711	92279	
Si	13	7461	30875	79388	118912	121020	90741	42504	
F	210	2230	4392	4393	0	843	0	3020	
Cl	729	7446	16130	32814	38125	49021	49831	15715	
NO ₃	846	9370	14905	34402	40243	51165	50443	15184	
SO ₄	1790	19326	38594	53455	41150	48408	32913	30480	
HCO ₃	4773	28712	53990	79599	98307	97053	91637	32372	

J. Jans
09/20/00

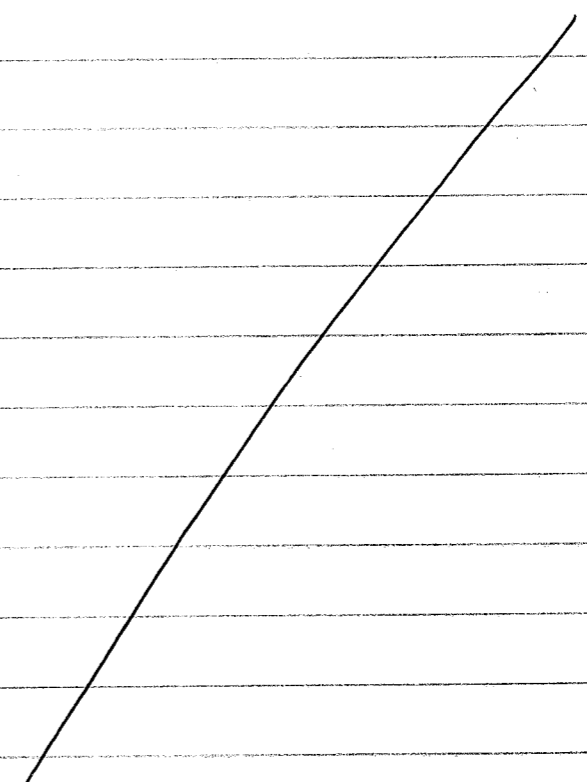
09/20/00

Table 17. Results of the Evaporative Concentration of a Simulated Well J-13 Water Under Conditions of Constant Temperature and RH

Species	Starting Solution (mg/L)	Final Solution 85%RH/90°C (mg/L)
Sample #	Initial J-13 Batch 1	J-13-01
DTN: LL990703005924.083		
Cl	730	14419
NO ₃	732	14085
SO ₄	1632	29783
F	208	3630
HCO ₃ ^o	4142	54614
Na	4032	76314
K	513	10832
Ca	5.0	36
Mg	2.0	0

19
19
18
17
13
19
21
7.2
0

* Total inorganic carbon given as bicarbonate.



J. Jans

09/20/00

09/20/00

Reconciliation of samples.

J.Y. 09/20/00

Study Name: ~~Syn-J13~~ Syn-J13
Chemistry Model: Syn-J13

Using OLS Sample Manager

① Synthetic J-13 Water
Sample Name: Syn-J13

After a few tries, set HCO_3^- to 100 mg/L
(original was 108 mg/L, as there must be errors in HCO_3^-)

Reconciled by proportion, adding 16.35% of each cation.

PH = 8.20529

Sample exported to
Esp by using

Stream ~~data~~ Manager

J.Y. 09/25/00

Sample Name
Syn-J13

J.Y. 09/25/00

J. Jones
2/14/02

Sample: Syn-J13.

Sample Name: Syn-J13

Template Reconcile Units LastResult Help Reconciled by, reduce HCO_3^-

Syn J13 Study
SYN J13 Model
Concentrations

Cations		Anions	
Input	Reconciled	Input	Reconciled
CA+2	6.4	CL-1	6.9
K+1	5.3	F-1	2.2
MG+2	2.2	HCO3-1	100*
NA+1	46.	NO3-1	46.
		SO4-2	18.1

Values in mg/l

Exported as
Syn-J13
PH = 8.205

Changed.
from 108 to 100

<PgDn>

Sample Name: A1

Note: HCO_3^- was reduced to 100 mg/L from 108 mg/L

* Average - J13 water.

Sample Name: Ave-J13

Reconciled with 11% cation proportion

Reconciled sample exported to ESP, same name

J. Jones

2/14/02

Sample Name: Ave-J13

Template Reconcile Ave-J13 Units LastResult Help Reconciled by Proportion

Syn_J13 Study
SYN_J13 Model
Concentrations

Values in mg/l					
Cations	Input	Reconciled	Anions	Input	Reconciled
CA+2	12.	13.3276	CL-1	6.7	6.69995
K+1	4.7	5.21997	F-1	4.4	4.39997
MG+2	1.9	2.1102	HCO3-1	139.	138.999
NA+1	46.	51.0891	NO3-1	8.8	8.79991
			SO4-2	17.	16.9999

Exported as
Ave-J13
PH=7.997

Si: ~~10~~ 573
= 2.546 mg/l

Aug. 09/20/00
mg/l

<PgDn>

* Synthetic Pore Water.

Sample Name: Syn-Pore

Reconciled by proportion 5.51% cation introduced.

J. James
8/14/02

Sample Name: Syn-Pore

Reconciled by proportion: 5.51% Cation

very good. basically within error.

PH = 7.997 (measured 7.95)

As $CaCO_3$ has the biggest error, I

reduce $CaCO_3$ by 4.30 which is the error range.

The reconcile by proportion: 3.86% of each ^{cation}

Now: $PH = 3.423$. impossible!!

Try $CaCO_3$ 20.3 - 1.0 mg/l 5.12% of each cation Required

PH = 7.996

Try $CaCO_3$ 20.3 - 2 = 18.3 mg/l 4.76% Cation required

PH = 7.99423

Try $CaCO_3$ 17.3 mg 4.36%

PH = 7.992

Try $CaCO_3$ 16.3 mg/l 3.96% , PH = 7.9897

J. James
8/14/02

Try HCO_3^- 15.2 mg/L ~~3.4%~~ ^{3.4%} ^{avg. 09/11/00} $\text{pH} = 7.987$

Try HCO_3^- 16.00 mg/L 3.86% $\text{pH} = 3.4136$

wrong !!

Try HCO_3^- 16.1 mg/L 3.40% $\text{pH} = 7.479$

Try HCO_3^- 15.9 mg/L 3.83% $\text{pH} = 3.413$

15.8 mg/L 3.74% $\text{pH} = 3.412$

15.1 3.67% $\text{pH} = 3.411$

15.4 3.63% $\text{pH} = 3.41$

Try HCO_3^- again 15.3 mg/L 3.60% $\text{pH} = 7.987$

15.2 3.56% $\text{pH} = 7.987$

Try HCO_3^- again, 14.3 mg/L 3.21% $\text{pH} = 3.405$

15.1 3.52% $\text{pH} = 7.9864$

15.0 3.48% $\text{pH} = 3.4086$

Use original HCO_3^- (20.3).

* Reconcile by 5.51% each cation. (proportion)

Export as Syn-Pore (original, $\text{HCO}_3^- = 20.3$) $\text{pH} = 7.997$.

Jim at OLI said I should not use proportion then I can find out which one causes the problem.

J. Jones
8/14/02

Sample Name: Syn-Pore.

Template Reconcile Units LastResult Help

SYN_J13 Study
SYN_J13 Model
Concentrations

Cations		Anions	
Input	Reconciled	Input	Reconciled
CA+2	57.	CL-1	76.6
K+1	4.	F-1	2.16
MG+2	11.8	HCO3-1	20.3
NA+1	8.56	NO3-1	10.7
		SO4-2	83.9

Sample Name
~~Ave-pore.~~
09/21/00
Syn-pore

$\text{pH} = 7.997$

<PgDn>

Reconciled by adding 5.51% each cation.

Exported to Esp: Syn-Pore.

* Average Pore Water.

Sample Name: Ave-Pore

NO_3^- Not analyzed, I assign the same value as in Syn-Pore. (10.7 mg/L)

As HCO_3^- in the Assay was calculated, I shall use HCO_3^- to balance the charge.

J. Jones
8/14/02

Sample: Ave-Pore

Template Reconcile Units LastResult Help

SYN_J13 Study
SYN_J13 Model
Concentrations

Values in mg/l

Cations	Input	Reconciled	Anions	Input	Reconciled
CA+2	101.	100.999	CL-1	117.	116.999
K+1	8.	7.99996	F-1	0.86	0.859995
MG+2	17.	16.9999	HCO3-1	200.	206.743
NA+1	61.3	61.2996	NO3-1	10.	9.9999
			SO4-2	116.	116.

Sample Name
Ave-Pore

PH = 8.205

<PgDn>

Reconciled by adding 6.744 mg/l HCO_3^- .
PH = 8.205

* Reconcile water from Table 16 of (ANL-EB5-MD-00001)
and from Table 17 (Rev 00C, 1991)

Sample Name: Table 16, added 2609.57 mg/l HCO_3^- , PH = 7.989

Sample Name: Table 17 added 2660.04 mg/l HCO_3^- , PH = 7.9977

Table 16 + Table 17 Exported to Esp Files. J. Young 2/14/02

Sample: Table 16

Template Reconcile Units LastResult Help

SYN_J13 Study
SYN_J13 Model
Concentrations

Values in mg/l

Cations	Input	Reconciled	Anions	Input	Reconciled
CA+2	6.	5.98434	CL-1	729.	727.097
K+1	535.	533.604	F-1	210.	209.452
MG+2			HCO3-1	4773.	7370.09
NA+1	4360.	4348.62	NO3-1	846.	843.794
			SO4-2	1790.	1785.33

Sample Name
Table 16
0.4629 mll
Si = 13 mg/l

PH = 7.984
added 2609.57
mg to balance

<PgDn>

Template Reconcile Units LastResult Help

SYN_J13 Study
SYN_J13 Model
Concentrations

Values in mg/l

Cations	Input	Reconciled	Anions	Input	Reconciled
CA+2	5.	4.98668	CL-1	730.	728.057
K+1	513.	511.636	F-1	208.	207.446
MG+2	2.	1.99468	HCO3-1	4142.	6791.06
NA+1	4032.	4021.27	NO3-1	732.	730.055
			SO4-2	1632.	1627.66

Sample Name
Table 17
Si = 0.

PH = 7.998

<PgDn>

Sample Table 17 Log. 09/25/00

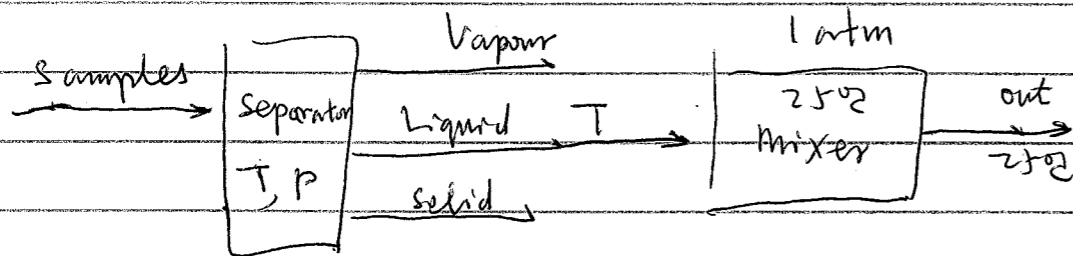
09/25/00

Simulation

* Evaporation at constant T & P

In Esp.

Process Build:



Isothermal: $T = 90^{\circ}\text{C}$; $P = 0.588021 \text{ atm}^*$

*: $P_{\text{H}_2\text{O}}(T=90^{\circ}\text{C}) = 525.76 \text{ mmHg}$, Page 3-4

Perry's Chem. Eng. Hand Book.

at 85% RH at 90°C , $525.76 * 0.85 = 446.896 \text{ mmHg}$
 $= 0.588021 \text{ atm}$

use Syn_J13 as input sample.

Chemistry Model: Syn_J13 (same)

Also, this model does not allow Regenerate the chemistry. I use a new one: "J13Z"

Regenerate the model, turn on all solid and add $11.3 \text{ mg/L Si} \rightarrow \frac{11.3}{28.08} = 0.4023 * 10^{-3} \text{ mol/L}$
 J. Young student

Save Results to spreadsheet Files

turn on all zero print (to have same format of print out).

After trying many times, I found it is better to export the Total species (Molecules) data.

In Spreadsheet: Two sheets, Summary^{sheet} and Data sheet.

Syn_J13_Evap_90.xls Summary_sheet Page 1 9/25/00

	after recalculated	from data sheet.		
	input 250C	Amount lost during evapor.	Amount left after evap	C of liquid after evap at 900C
	mg/L	mg	mg	mg/L
Ca	7.446	7.4342	0.0118	2.79E+01
Cl	6.9	3.017E-09	6.9	1.63E+04
F	2.2	1.3161431	0.883857	2.09E+03
HCO3	100	78.08732	21.91268	5.18E+04
K	6.16657	0	6.16657	1.46E+04
Mg	2.5597	2.560005	-0.000305	-7.21E-01
Na	53.5215	0	53.5215	1.27E+05
NO3	46	2.055E-08	46	1.09E+05
SO4	18.1	0	18.1	4.28E+04
Si	11.3	0	11.3	2.67E+04
pH	8.08679			10.9112
Sum (mg/L)				3.90E+05
Density (kg/m^3)	0.99706			1.268084
Volume of liquid (m^3/hr or m^3)				4.23E-07
Note: pH=	8.205	(before SiO2 introduced for input)		
Moles (mM):	0.40242			

J. Young

3/9/02

09/25/00

Exported by Esp

Calculated to see contributions to elements or compon.

Stream	Syn_J13	V_Syn_J13	L_Syn_J13	S_Syn_J13	Out	Species	FW	amount to vapour mole	amount to Solid mole	Total lost in Evapora mg
Phase	Aqueous	Vapor	Aqueous	Solid	Mixed					
Temperature, C	25	90	90	90	25					
Pressure, atm	1	0.588021	0.588021	0.588021	1					
pH	8.08679		10.9112		11.9083					
Total mol/hr	55.5142	55.4931	0.0212966	2.91E-04	0.0213019					
Flow Units	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr					
H2O	55.5115	55.492	0.0195573		0.0195519	Ca	40		1.86E-04	7.4342
H2F2	3.72E-05	3.44E-22	5.54E-06			CL	35.5	8.50E-14		3.0173E-09
CO2	6.11E-04		1.42E-11		2.56E-13	F	19	6.91E-10	6.93E-05	1.31614313
H2SO4						HCO3	61	0.0017249	1.51E-04	78.08732
HCL		8.50E-14	3.69E-05		7.37E-06	K				0
HF	1.44E-09	6.91E-10	2.00E-13		7.76E-15	Mg	24.3		1.05E-04	2.560005
HNO3	3.02E-04	3.31E-13	3.38E-16			Na				0
SICL4						NO3	62	3.31E-13		2.0549E-08
SIF4	1.03E-05					SO4				0
SO3						Si				0
H2SIO3	1.96E-04		6.14E-08		1.26E-08					
KCL	2.24E-10		1.58E-04		1.58E-04					
KHSO4			3.23E-17							
MGCO3	6.28E-07		3.83E-11		2.70E-11					
MGH2SIO4	1.38E-09		2.74E-10		2.88E-10					
MGSO4	7.21E-07		1.35E-13		4.16E-13					
NAF	1.83E-07		3.55E-05		4.05E-05					
NAHCO3	1.36E-06		2.43E-06		1.04E-07					
NAHSIO3	9.10E-07		3.46E-04		3.95E-04					
NANO3	2.79E-08		7.42E-04		7.42E-04					
CASO4	2.50E-06		1.74E-12		1.20E-12					
CAH2SIO4	2.54E-10		2.00E-10		4.40E-11					
SIO2	1.95E-04		2.20E-07		1.46E-08					
CACO3	2.48E-06		7.81E-10	1.51E-04	8.84E-11					
H2CO3										
H6F6										
KMGCL3	6.49E-05		2.02E-11		1.71E-11					
KOH										
NA3HSO42										
NA6SO42CO3	9.26E-05		9.42E-05		9.12E-05					
MGOH2				1.05E-04						
NAOH					5.21E-06					
CAOH2										
CA2CL2O.2H2C										
CACL2.1H2O										
CACL2.2H2O										
CACL2.4H2O										
CACL2.6H2O										
CACL2			1.10E-10		5.80E-11					
CAF2				3.46E-05	9.01E-10					
CANO32.3H2O										
CANO32.4H2O										
CANO32	1.81E-04									
CASO4.2H2O										
K2CO3.1.5H2O										
K2CO3	4.64E-05									
K2SO4.1H2O										
K2SO4										

Contributed from different rows.

J. Jans
3/14/02

09/25/00

K3NASO42				
KF.2H2O				
KF.4H2O				
KF				
KHCO3				
KMGCL3.2H2O				
KNO3				
KOH.1H2O				
KOH.2H2O				
MGCL2.2H2O				
MGCL2.4H2O				
MGCL2.6H2O				
MGCL2				
MGCLOH				
MGCO3.3H2O				
MGF2				
MGNO32.2H2O				
MGNO32.6H2O				
MGNO32	3.91E-05			
MGSO4.1H2O				
MGSO4.6H2O				
MGSO4.7H2O				
MGSO4OH.0.5H				
MGSO4OH				
NA2CO3.10H2C				
NA2CO3.1H2O				
NA2CO3.7H2O				
NA2CO3	8.85E-04	2.63E-04		2.68E-04
NA2SIO3.5H2O				
NA2SIO3.6H2O				
NA2SIO3.9H2O				
NA2SIO3		5.62E-05		7.76E-06
NA2SO4.10H2C				
NA2SO4				
NA3FSO4				6.07E-06
NACL				2.95E-05
NAHF2				
NAHSO4				
NAOH.1H2O				
Total g/hr	1000.32	999.755	0.536501	0.023983
Volume, m3/hr	0.0010033	2.79744	4.23E-07	0.03E-09
Enthalpy, cal/hr	-3.79E+06	-3.18E+06	-1713.45	-76.6669
Vapor fraction		1		
Solid fraction			1	2.85E-04
Organic fraction				
Osmotic Pres, a	0.135279		265.473	222.626
Redox Pot, volts				
E-Con, 1/ohm-c	3.18E-04		0.4274	0.178569
E-Con, cm2/ohr	64.4057		67.7448	41.0006
Abs Visc, cP	0.891946		1.02723	2.83186
Rel Visc	1.00138		3.26916	3.1793
Ionic Strength	0.0035189		7.29586	6.81646

$$\text{density} = \frac{0.5365 \times 10^{-6} \text{ t}}{0.423 \times 10^{-6} \text{ m}^3} = 1.268 \frac{\text{t}}{\text{m}^3}$$

J. J. 12/04/00

J. Jans
3/14/02

Note: OLI does not print out concentrations of element or basic compound. I did it the following way:

f.y. 09/15/00

$$\text{Weight}(i) =$$

$$\text{Weight}(i, \text{in liquid}) = \text{Weight}(i, \text{input}) - \text{Weight}(i, \text{vapour}) - \text{Weight}(i, \text{solid})$$

As there are only a few vapour and solid species.

f.y. 09/15/00

$$C_i(90^\circ\text{C}) = \frac{\text{Weight}(i, \text{in liquid}) \text{ at } 90^\circ\text{C}}{\text{Volume at } 90^\circ\text{C}}$$

$$C_i(25^\circ\text{C}) = \frac{\text{Weight}(i, \text{in liquid}) \text{ at } 90^\circ\text{C}}{\text{Volume cooled to } 25^\circ\text{C}}$$

f.y. 09/15/00

Working with different samples. (Evap. at 90°C, 85% RH)

1. Syn-J13: adding SiO₂: 11.3 mg/L of Si → 0.40242 × 10⁻³ mol/L
 Saved spreadsheet file as Syn-J13-Evap-90.xls
 f.y. 09/26/00

2. Ave-J13: Adding SiO₂: 57.3/23.03 (of Si) ⇒ 4.025E-4 mol/L
 2.04E-3

Spreadsheet file saved as Ave-J13-Evap-90.xls

3. Syn-pore: specify: SiO₂ = 22.2 mg/L → 0.3641E-3 mol/L

spreadsheet file saved as: Syn-pore-Evap-90.xls

4. Ave-pore: specify: SiO₂ = 70.6 mg/L → 1.175E-3 mol/L

Spreadsheet file saved as: Ave-Pore-Evap-90.xls

5. Table 17: specify: SiO₂ = 0

spreadsheet file saved as: Table17-Evap-90.xls

~~6. Table 16: specifying~~ f.y. 09/25/00

* Note: File Directory C:\work\J13-Water

J. Jans

8/19/02

working with Different samples
Boiling at 1 atm

1. Table 16 Sample

adding Si: 1.3 mg/L

① 101°C: spreadsheet file saved as Table16-Evap-101.XLS

② 104°C | Table16-Evap-104.XLS

③ 108°C | -108.XLS

④ 112°C | -112.XLS

⑤ 120°C spreadsheet file saved as Table16-Evap-120.XLS

⑥ 110°C spreadsheet file saved as Table16-Evap-120.XLS

⑦ 111°C spreadsheet file saved as Table16-Evap-111.XLS

July
09/27/00

2. Syn-J13 sample

adding Si: 11.3 mg/L

① 101°C: spreadsheet file saved as Syn-J13-Evap-101.XLS

② 104°C | -104.XLS

③ 108°C | -108.XLS

④ 112°C | -112.XLS

⑤ 120°C spreadsheet file saved as Syn-J13-Evap-120.XLS

July
09/25/00

Note: All files in directory C:\work\J13-Water

3. Ave-J13 sample. adding SiO₂: 57.3 mg/L of Si ⇒ ~~4.025E-3 mol/L~~

July
09/26/00

~~4.025E-3 mol/L~~
2.04E-3 mol/L

① 101°C spreadsheet file saved as Ave-J13-Evap-101.XLS

② 104°C | -104.XLS

③ 108°C | -108.XLS

④ 112°C | -112.XLS

⑤ 120°C spreadsheet file saved as Ave-J13-Evap-120.XLS

Note: at 108°C Na₂SO₄ were found to be solid.
only at this temperature.

4. Syn-Pore sample: adding SiO₂: 22.2 mg/L of SiO₂ ⇒ 0.369E-3 mol/L

① 101°C spreadsheet file saved as Syn-Pore-Evap-101.XLS

② 104°C | -104.XLS

③ 108°C | -108.XLS

④ 112°C | -112.XLS

⑤ 120°C spreadsheet file saved as Syn-Pore-Evap-120.XLS

5. Ave-Pore sample: adding SiO₂: 70.6 mg/L of SiO₂ ⇒ 1.171E-3 mol/L

① 101°C spreadsheet file saved as Ave-Pore-Evap-101.XLS

② 104°C | -104.XLS

③ 108°C | -108.XLS

④ 112°C | -112.XLS

⑤ 120°C spreadsheet file saved as Ave-Pore-Evap-120.XLS

All files were printed out and filed in a binder.

Note: All files in Pages 19-20 are in directory:

C:\work\J13_water

All Results are consolidated into one file, 6 sheets.

File name: J13-Water-Evaporation.xls

See pages 21-26

J.Y. 09/27/00

	Conc of species (mg/L) in liquid if sampled at high temperature and analyzed at 25°C						
	Input	Evaporation under Boiling Condition (1 atm)					Evaporation at Const T and RH
Temperature °C	25	101	104	108	112	120	90oC, 85%RH
Ca	7.45E+00	6.76E+00	2.60E+01	4.94E+01	7.34E+01	1.17E+02	2.95E+01
Cl	6.90E+00	3.76E+03	1.48E+04	2.91E+04	4.21E+04	6.70E+04	1.73E+04
F	2.20E+00	1.20E+03	2.78E+03	3.55E+03	3.59E+03	2.32E+03	2.21E+03
HCO3	1.00E+02	1.01E+04	4.51E+04	7.25E+04	7.29E+04	2.44E+04	5.49E+04
K	6.17E+00	3.36E+03	1.32E+04	2.60E+04	3.76E+04	5.99E+04	1.54E+04
Mg	2.56E+00	-1.66E-01	-6.54E-01	-1.29E+00	-1.86E+00	-2.96E+00	-7.64E-01
Na	5.35E+01	2.92E+04	1.15E+05	1.80E+05	2.29E+05	2.88E+05	1.34E+05
NO3	4.60E+01	2.51E+04	9.87E+04	1.94E+05	2.80E+05	4.47E+05	1.15E+05
SO4	1.81E+01	9.87E+03	3.88E+04	1.30E+04	7.03E+03	6.40E+03	4.53E+04
Si	1.13E+01	6.16E+03	2.42E+04	4.76E+04	6.89E+04	1.10E+05	2.83E+04
pH after cooled to 25oC	8.09E+00	1.18E+01	1.21E+01	1.24E+01	1.27E+01	1.27E+01	1.19E+01
pH at T	8.09E+00	1.06E+01	1.08E+01	1.10E+01	1.10E+01	1.10E+01	1.09E+01
Sum of salt (mg/L)	2.54E+02	8.87E+04	3.52E+05	5.66E+05	7.41E+05	1.00E+06	4.13E+05
Dens at T (kg/m ³)	9.97E-01	1.03E+00	1.22E+00	1.36E+00	1.48E+00	1.65E+00	1.27E+00
Dens at 25oC (kg/m ³)	9.97E-01	1.07E+00	1.29E+00	1.47E+00	1.61E+00	1.83E+00	1.34E+00
V of liquid at 25oC (m ³)	1.00E-03	1.83E-06	4.66E-07	2.37E-07	1.64E-07	1.03E-07	3.99E-07
V fraction remaining	1.00E+00	1.83E-03	4.65E-04	2.37E-04	1.63E-04	1.03E-04	3.98E-04

File location: C:\work\J13_water\

Should be t/m³, see page 15.

J.Y. 12/04/00

J.Y.

8/19/02

1.27 t/m³
see page 15

J.Y.
12/04/00

	Conc of species (mg/L) in liquid if sampled at high temperature and analyzed at 25 °C							Evaporation at Const T and RH
	Input	Evaporation under Boiling Condition (1 atm)						
Temperature °C	25	101	104	108	112	120	90oC, 85%RH	
Ca	1.33E+01	1.33E+01	5.38E+01	1.04E+02	1.56E+02	4.79E+02	6.31E+01	
Cl	6.70E+00	3.91E+03	1.63E+04	3.19E+04	4.81E+04	1.29E+05	1.94E+04	
F	4.40E+00	5.39E+02	1.68E+03	2.84E+03	3.63E+03	2.66E+03	1.61E+03	
HCO3	1.39E+02	1.20E+03	1.37E+04	3.69E+04	5.59E+04	2.51E+04	2.37E+04	
K	5.22E+00	3.04E+03	1.27E+04	2.49E+04	3.75E+04	1.15E+05	1.51E+04	
Mg	2.11E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	-7.54E-01	
Na	5.11E+01	2.98E+04	1.25E+05	2.14E+05	2.84E+05	2.91E+05	1.48E+05	
NO3	8.80E+00	5.13E+03	2.15E+04	4.19E+04	6.32E+04	1.93E+05	2.55E+04	
SO4	1.70E+01	9.91E+03	4.15E+04	2.07E+04	7.50E+03	2.38E+03	4.92E+04	
Si	5.73E+01	2.57E+04	9.93E+04	1.85E+05	2.46E+05	2.20E+05	1.11E+05	
pH after cooled to 25oC	7.92E+00	1.09E+01	1.12E+01	1.15E+01	1.16E+01	1.16E+01	1.13E+01	
pH at T	7.92E+00	1.00E+01	1.05E+01	1.07E+01	1.09E+01	1.10E+01	1.07E+01	
Sum of salt (mg/L)	3.05E+02	7.92E+04	3.31E+05	5.59E+05	7.47E+05	9.78E+05	3.93E+05	
Dens at T (kg/m^3)	9.97E-01	1.05E+00	1.33E+00	1.61E+00	1.81E+00	1.86E+00	1.40E+00	
Dens at 25oC (kg/m^3)	9.97E-01	1.10E+00	1.41E+00	1.73E+00	1.98E+00	2.04E+00	1.48E+00	
V of liquid at 25oC (m^3)	1.00E-03	1.72E-06	4.10E-07	2.10E-07	1.39E-07	4.55E-08	3.46E-07	
V fraction remaining	1.00E+00	1.71E-03	4.09E-04	2.09E-04	1.39E-04	4.54E-05	3.45E-04	

File location: c:\work\j13_water

t/m³. see page 21

J.Y. 12/04/00

[Handwritten signature]
8/10/02

	Conc of species (mg/L) in liquid if sampled at high temperature and analyzed at 25 °C							Evaporation at Const T and RH
	Input	Evaporation under Boiling Condition (1 atm)						
Temperature °C	25	101	104	108	112	120	90oC, 85%RH	
Ca	6.01E+01	1.17E+04	3.60E+04	6.22E+04	8.03E+04	1.24E+05	3.94E+04	
Cl	7.66E+01	3.87E+04	1.18E+05	1.89E+05	2.44E+05	3.25E+05	1.31E+05	
F	2.16E+00	1.42E+00	7.31E-01	1.42E+00	3.31E+00	1.09E+01	-1.25E-01	
HCO3	2.03E+01	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	-2.41E+00	
K	4.22E+00	2.13E+03	6.47E+03	1.04E+04	1.35E+04	2.07E+04	7.22E+03	
Mg	1.25E+01	4.25E+03	1.24E+04	1.73E+04	2.24E+04	3.38E+04	1.44E+04	
Na	9.03E+00	4.56E+03	1.39E+04	2.23E+04	2.88E+04	4.44E+04	1.55E+04	
NO3	1.07E+01	5.40E+03	1.64E+04	2.64E+04	3.41E+04	5.26E+04	1.83E+04	
SO4	8.39E+01	4.24E+04	1.29E+05	2.07E+05	2.67E+05	4.12E+05	1.44E+05	
SiO2	2.22E+01	8.35E+02	4.75E+02	2.93E+02	2.01E+02	1.29E+02	3.41E+02	
pH after cooled to 25oC	7.82E+00	8.26E+00	7.86E+00	7.70E+00	7.55E+00	7.55E+00	7.88E+00	
pH at T	7.82E+00	7.07E+00	6.60E+00	6.23E+00	5.93E+00	5.50E+00	6.80E+00	
Sum of salt (mg/L)	3.02E+02	1.10E+05	3.32E+05	5.35E+05	6.91E+05	1.01E+06	3.70E+05	
Dens at T (kg/m^3)	9.97E-01	1.01E+00	1.10E+00	1.17E+00	1.23E+00	1.31E+00	1.12E+00	
Dens at 25oC (kg/m^3)	9.97E-01	1.05E+00	1.15E+00	1.23E+00	1.30E+00	1.39E+00	1.16E+00	
V of liquid at 25oC (m^3)	1.00E-03	1.98E-06	6.52E-07	4.05E-07	3.14E-07	2.03E-07	5.84E-07	
V fraction remaining	1.00E+00	1.97E-03	6.50E-04	4.04E-04	3.13E-04	2.03E-04	5.83E-04	

File location ~~J13~~ J.Y. 09/28/00

c:\work\j13_water

t/m³, see page 21

J.Y. 12/04/00

	Conc of species (mg/L) in liquid if sampled at high temperature and analyzed at 25 °C						
	Input	Evaporation under Boiling Condition (1 atm)					Evaporation at Const T and RH
Temperature °C	25	101	104	108	112	120	90oC, 85%RH
Ca	1.01E+02	3.41E+03	1.11E+04	1.85E+04	9.31E+04	2.53E+05	1.21E+04
Cl	1.17E+02	3.47E+04	1.17E+05	1.91E+05	2.55E+05	3.60E+05	1.31E+05
F	8.60E-01	2.33E+00	1.11E+00	1.53E+00	2.46E+00	2.39E+01	5.56E-01
HCO3	2.07E+02	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	-1.04E+02
K	8.00E+00	2.38E+03	7.98E+03	1.30E+04	6.37E+04	1.72E+05	8.95E+03
Mg	1.70E+01	2.95E+02	5.93E+02	5.97E+02	1.09E+03	1.03E+03	1.12E+03
Na	6.13E+01	1.82E+04	6.11E+04	9.99E+04	4.88E+05	1.32E+06	6.86E+04
NO3	1.00E+01	2.97E+03	9.97E+03	1.63E+04	7.96E+04	2.15E+05	1.12E+04
SO4	1.16E+02	3.45E+04	1.16E+05	1.89E+05	9.24E+05	2.49E+06	1.30E+05
SiO2	7.06E+01	1.05E+03	6.19E+02	3.60E+02	2.58E+02	3.62E+02	4.72E+02
pH after cooled to 25oC	7.32E+00	8.39E+00	7.86E+00	7.59E+00	7.86E+00	8.05E+00	7.86E+00
pH at T	7.32E+00	7.60E+00	7.18E+00	6.84E+00	6.37E+00	5.84E+00	7.28E+00
Sum of salt (mg/L)	7.09E+02	9.75E+04	3.24E+05	5.29E+05	1.90E+06	4.81E+06	3.63E+05
Dens at T (kg/m^3)	9.97E-01	1.00E+00	1.08E+00	1.15E+00	1.28E+00	1.49E+00	1.11E+00
Dens at 25oC (kg/m^3)	9.97E-01	1.04E+00	1.14E+00	1.22E+00	1.35E+00	1.58E+00	1.15E+00
V of liquid at 25oC (m^3)	1.00E-03	3.37E-06	1.00E-06	6.13E-07	1.26E-07	4.65E-08	8.94E-07
V fraction remaining	1.00E+00	3.36E-03	1.00E-03	6.11E-04	1.25E-04	4.64E-05	8.91E-04

File location: C:\work\J13-water\

t/m³, see page 21, J.Y. 12/04/00

	Conc of species (mg/L) in liquid if sampled at high temperature and analyzed at 25 °C						
	Input	Evaporation under Boiling Condition (1 atm)					Evaporation at Const T and RH
Temperature °C	25	101	104	108	112	120	90oC, 85%RH
Ca	6.00E+00	3.62E-01	-2.67E+00	-6.58E+00	-3.89E+01	-3.66E+01	
Cl	7.27E+02	7.39E+02	2.30E+04	5.62E+04	5.40E+04	5.48E+04	
F	2.09E+02	2.13E+02	6.44E+03	1.57E+04	8.12E+04	8.16E+04	
HCO3	7.37E+03	7.45E+03	1.09E+05	1.39E+05	5.41E+04	2.70E+04	
K	5.33E+02	5.42E+02	1.69E+04	4.12E+04	4.59E+04	4.91E+04	
Mg	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	
Na	4.35E+03	4.42E+03	1.37E+05	3.36E+05	7.04E+05	6.49E+05	
NO3	8.44E+02	8.57E+02	2.67E+04	6.52E+04	3.86E+05	3.63E+05	
SO4	1.79E+03	1.81E+03	5.64E+04	1.38E+05	8.16E+05	7.67E+05	
Si	1.30E+01	1.32E+01	4.11E+02	1.00E+03	1.82E+03	1.77E+03	
pH after cooled to 25oC	7.98E+00	8.01E+00	1.01E+01	1.02E+01	1.01E+01	1.05E+01	
pH at T	7.98E+00	7.89E+00	1.01E+01	1.02E+01	1.04E+01	1.04E+01	
Sum of salt (mg/L)	1.58E+04	1.60E+04	3.77E+05	7.92E+05	2.14E+06	1.99E+06	
Dens at T (kg/m^3)	9.97E-01	9.69E-01	1.18E+00	1.27E+00	3.87E+00	4.60E+00	
Dens at 25oC (kg/m^3)	9.97E-01	1.01E+00	1.26E+00	1.37E+00	3.09E+00	2.90E+00	
V of liquid at 25oC (m^3)	1.01E-03	9.84E-04	3.16E-05	1.29E-05	2.19E-06	2.33E-06	
V fraction remaining	1.00E+00	9.74E-01	3.13E-02	1.28E-02	2.16E-03	2.30E-03	

Back to calculate again

good

110 111 112, 09/27

-10.8389 -39.2772 -38.9486

92498.92 53973.61 53985.89

25909.74 81528.84 81154.49

73492.5 58667.99 54122.61

67806.53 45601.28 45909.76

0 0 0

150894 712212.9 703523.2

107345.5 388991.3 385737.1

894.3439 822884 816000

1653.818 1828.242 1818.21

10.094 9.98492 10.0571

10.1871 10.3856 10.3898

520484.5 2165649 2142212

1.260839 3.785547 3.873148

1.378877 3.12606 3.09445

7.86E-06 2.17E-06 2.19E-06

* Density(112oC)=3.87>Density(25oC)=3.09?, Right column shows 110oC no problem, 111oC problem started

File location: C:\work\J13-water\

t/m³, see page 21, J.Y. 12/04/00

	Conc of species (mg/L) in liquid if sampled at high temperature and analyzed at 25 °C						Evaporation at Const T and RH
	Input	Evaporation under Boiling Condition (1 atm)					
Temperature °C	25	101	104	108	112	120	90oC, 85%RH
Ca							-2.56E+00
Cl							2.97E+04
F							4.66E+03
HCO3							1.27E+05
K							2.09E+04
Mg							-1.17E+00
Na							1.64E+05
NO3							2.98E+04
SO4							6.65E+04
Si							0.00E+00
pH after cooled to 25oC							1.03E+01
pH at T							1.02E+01
Sum of salt (mg/L)							4.43E+05
Dens at T (kg/m^3)							1.22E+00
Dens at 25oC (kg/m^3)							1.30E+00
V of liquid at 25oC (m^3)	1.01E-03						2.45E-05
V fraction remaining	1.00E+00						2.42E-02

File location: c:\work\J13 water

t/m³, see page 21

J.Y. 12/04/00

J.Y. 09/28/00

OLI Comments:

In the process Building stage, I specified

Flow (water) = 55.5087 mols/hr

Flow (total) = 55.8188 mols/hr

Everytime the program ran, the output flow rate is changed slightly? Why? (to: total = ~~55.695~~; H₂O = 55.6955 = 55.8597;

See below:

J.Y. 09/28/00

Table16_Evap_101.xls Data_sheet Page 1/2 9/28/00

Stream	Table16	V_Syn_J13	L_Syn_J13	S_Syn_J13	Out
Phase	Mixed	Vapor	Aqueous	Solid	Mixed
Temperature, C	25	101	101	101	25
Pressure, atm	1	1	1	1	1
pH	7.98174		7.88851		8.01333
Total mol/hr	55.8597	1.45609	54.3972	1.41E-04	54.4033
Flow Units	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr
H2O	55.6955	1.45566	54.2338		54.2396
H2F2	5.11E-03	5.58E-24	5.26E-03		0.00523388
CO2	3.69E-02	0.00042869	3.01E-02		3.63E-02
H2SO4					
HCL	0.0208576	2.19E-17	2.06E-02		2.09E-02
HF	1.19E-07	1.23E-11	6.48E-07		1.13E-07
HNO3	1.38E-02	4.47E-16	1.38E-02		0.0138379
SICL4	9.051E-06	1.9139E-28	6.8184E-05		9.6158E-06
SIF4					

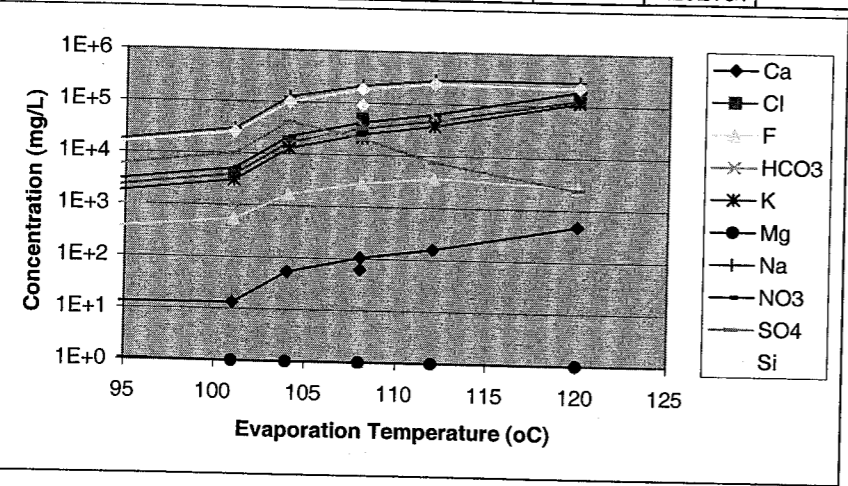
J.Y. 09/28/00

Nov. 20/00.

Plotting results for J-13 Average Water

J13_Water_Evaporation_bobby.xls Ave_J13 Page 1/1 11/20/00

Conc of species (mg/L) in liquid if sampled at high temperature and analyzed at 25 °C	Evaporation under Boiling Condition (1 atm)						Table 16 DOE Report	Evaporation at Const T and RH
	Input	25	101	104	108	112		
Temperature °C	25	101	104	108	112	120	108	90°C, 85%RH
Ca	1.33E+01	1.33E+01	5.38E+01	1.04E+02	1.56E+02	4.79E+02	6.20E+01	6.31E+01
Cl	6.70E+00	3.91E+03	1.63E+04	3.19E+04	4.81E+04	1.29E+05	4.98E+04	1.94E+04
F	4.40E+00	5.39E+02	1.68E+03	2.84E+03	3.63E+03	2.66E+03	1.00E+00	1.61E+03
HCO3	1.39E+02	1.20E+03	1.37E+04	3.69E+04	5.59E+04	2.51E+04	9.16E+04	2.37E+04
K	5.22E+00	3.04E+03	1.27E+04	2.49E+04	3.75E+04	1.15E+05	2.15E+04	1.51E+04
Mg	2.11E+00	1.00E+00	1.00E+00	1.00E+00	1.00E+00	1.00E+00	1.00E+00	-7.54E-01
Na	5.11E+01	2.98E+04	1.25E+05	2.14E+05	2.84E+05	2.91E+05	1.91E+05	1.48E+05
NO3	8.80E+00	5.13E+03	2.15E+04	4.19E+04	6.32E+04	1.93E+05	5.04E+04	2.55E+04
SO4	1.70E+01	9.91E+03	4.15E+04	2.07E+04	7.50E+03	2.38E+03	3.29E+04	4.92E+04
Si	5.73E+01	2.57E+04	9.93E+04	1.85E+05	2.46E+05	2.20E+05	9.07E+04	1.11E+05
pH after cooled to 25°C	7.92E+00	1.09E+01	1.12E+01	1.15E+01	1.16E+01	1.16E+01		1.13E+01
pH at T	7.92E+00	1.00E+01	1.05E+01	1.07E+01	1.09E+01	1.10E+01		1.07E+01
Sum of salt (mg/L)	3.05E+02	7.92E+04	3.31E+05	5.59E+05	7.47E+05	9.78E+05		3.93E+05
Dens at T (kg/m³)	9.97E-01	1.05E+00	1.33E+00	1.61E+00	1.81E+00	1.86E+00		1.40E+00
Dens at 25°C (kg/m³)	9.97E-01	1.10E+00	1.41E+00	1.73E+00	1.98E+00	2.04E+00		1.48E+00
V of liquid at 25°C (m³)	1.00E-03	1.72E-06	4.10E-07	2.10E-07	1.39E-07	4.55E-08		3.46E-07
Volume Factor	1.00E+00	5.85E+02	2.45E+03	4.78E+03	7.20E+03	2.20E+04		2.90E+03

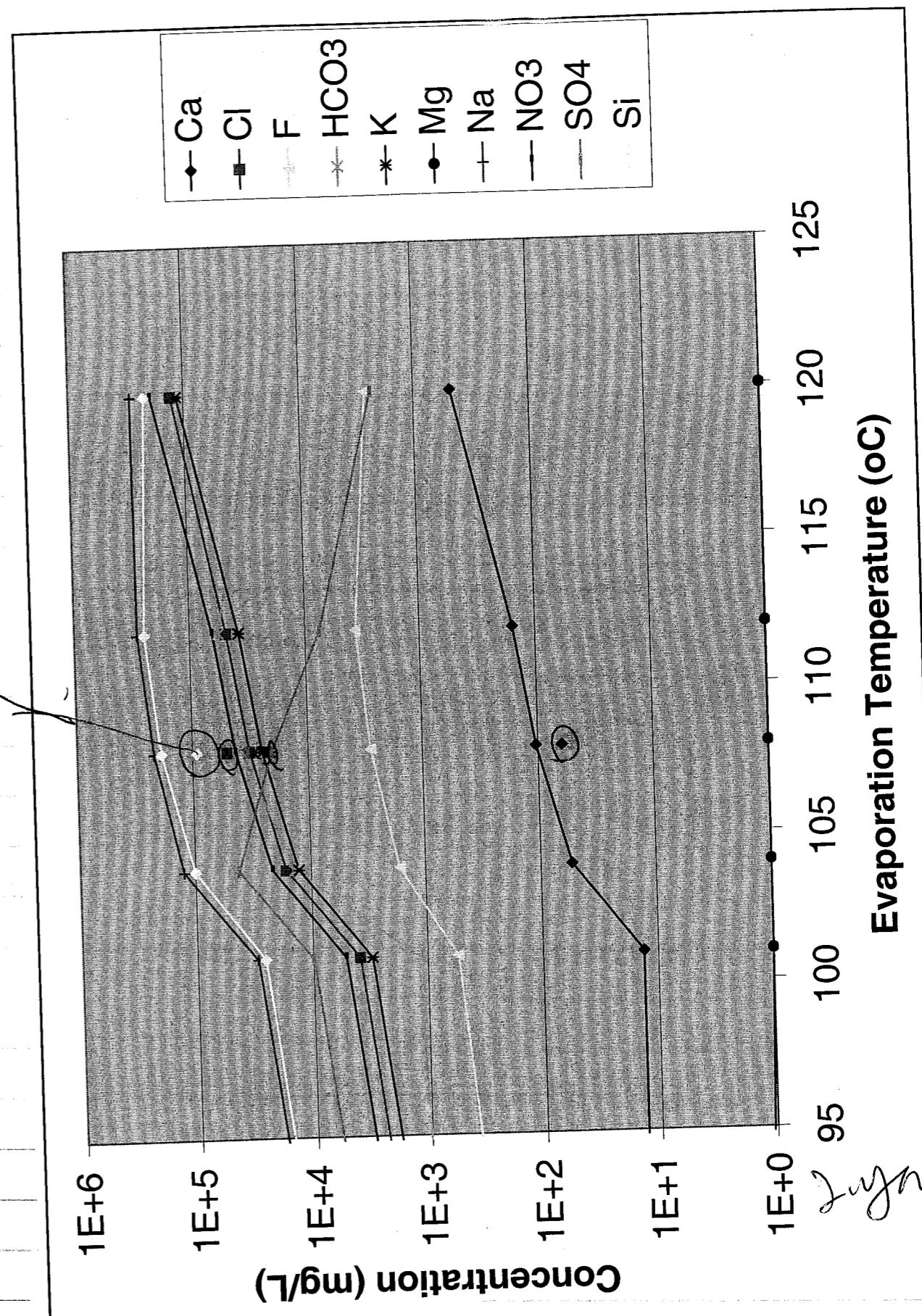


See page 21
July 12/14/00

DOE Results are similar. They are similar with our results.

July 11/20/00

DOE Results



July 8/14/00

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STREAM SECTION

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*Lizano
3/19/02*

CRIIICL3IN moles	PH	CRIIICLION moles	CRIIIION moles	CRIIICL2ION moles	CROH3AQ moles
0.0000	0.4163	0.0000	0.0000	0.0000	0.0000
0.2500	0.4104	0.7557E-01	0.1728	0.1660E-02	0.2121E-19
0.5000	0.3542	0.1832	0.3118	0.4979E-02	0.1556E-19
0.7500	0.2899	0.3276	0.4120	0.1041E-01	0.1051E-19
1.000	0.2254	0.5074	0.4745	0.1811E-01	0.7111E-20
1.250	0.1629	0.7168	0.5053	0.2792E-01	0.4872E-20
1.500	0.1027	0.9488	0.5117	0.3947E-01	0.3377E-20
1.750	0.4449E-01	1.197	0.5002	0.5236E-01	0.2360E-20
2.000	-0.1211E-01	1.457	0.4764	0.6622E-01	0.1658E-20
2.250	-0.6741E-01	1.725	0.4444	0.8075E-01	0.1168E-20
2.500	-0.1217	1.997	0.4075	0.9575E-01	0.8224E-21
2.750	-0.1752	2.271	0.3682	0.1111	0.5786E-21
3.000	-0.2280	2.545	0.3284	0.1267	0.4062E-21
3.250	-0.2802	2.818	0.2896	0.1425	0.2844E-21
3.500	-0.3318	3.089	0.2528	0.1586	0.1985E-21
3.750	-0.3829	3.356	0.2188	0.1750	0.1382E-21
4.000	-0.4334	3.620	0.1880	0.1917	0.9605E-22
4.250	-0.4831	3.881	0.1606	0.2088	0.6667E-22
4.500	-0.5321	4.137	0.1367	0.2263	0.4627E-22
4.750	-0.5803	4.390	0.1160	0.2442	0.3215E-22
5.000	-0.6274	4.639	0.9834E-01	0.2627	0.2240E-22
5.250	-0.6735	4.885	0.8344E-01	0.2817	0.1567E-22
5.500	-0.7184	5.128	0.7097E-01	0.3013	0.1102E-22
5.750	-0.7621	5.368	0.6060E-01	0.3214	0.7795E-23
6.000	-0.8043	5.606	0.5203E-01	0.3421	0.5557E-23
6.250	-0.8452	5.842	0.4496E-01	0.3633	0.3996E-23
6.500	-0.8845	6.076	0.3917E-01	0.3851	0.2900E-23
6.750	-0.9222	6.308	0.3445E-01	0.4074	0.2126E-23
7.000	-0.9582	6.539	0.3060E-01	0.4303	0.1575E-23
7.250	-0.9926	6.769	0.2750E-01	0.4536	0.1181E-23
7.500	-1.025	6.998	0.2502E-01	0.4775	0.8959E-24
7.750	-1.056	7.225	0.2307E-01	0.5018	0.6881E-24
8.000	-1.085	7.452	0.2158E-01	0.5266	0.5354E-24

Page A-3

*Lizano
3/19/02*

10
9/17/98
9/18/98

Speciation modeling of simulated pit solutions

Objective: The objective is to understand the speciation in concentrated chloride solutions in pits of stainless steels and Ni-base alloys. Such an understanding will aid in an understanding of repassivation mechanisms in pits and in understanding the analyses performed.

Approach: Used ESP version 6.0 from DLI Systems, Inc. to determine speciation in $CrCl_3$, $FeCl_2$ and $NiCl_2$ and mixtures.

Chemistry Model: $FeCl_2$

Specified Inflows:

H_2O	$FeCl_2$	H_2SO_4
HCl	$FeSO_4$	$NaCl$
$NaOH$	$FeCO_3$	$CrCl_3$
$NiCl_2$		

$Fe^{II}Cl_2 = 0$
 $Ni^{II}Cl_2 = 0$
 $Cr^{III}Cl_3 = \text{variable}$
 $HCl = 0.5M$

Temp: 25°C

Output of survey: $FeCl_2$ lis saved as excel file $crcl_3sur.txt$.

No precipitation was noted for $CrCl_3$ up to 8m. Hence the conc. was increased to 15m. NO HCl no precipitation was seen even in this case. Output saved as $crcl_3sur2.txt$

J. Jones
Staylor

N. Sridhar

9/17/98

9/17/98
9/18/98

$CrCl_3 + 0.5M HCl$ survey

SURVEY: $CrCl_3$
 CHEMISTRY MODEL: $FeCl_2$
 THIS FILE NAME: $FeCl_2.LIS$
 DATE: 9/17/98

ESP V-6.0 SURVEY-VA 9/17/98 PAGE 2

CRIIICL3IN lmoles	PH lmoles	CRIIICLION lmoles	CRIIIION lmoles	CRIIICL2ION lmoles	CROH3AQ lmoles
0	0.4163	0	0	0	0
0.25	0.4103	7.56E-02	0.1728	1.66E-03	2.12E-20
0.5	0.354	0.1832	0.3118	4.98E-03	1.55E-20
0.75	0.2896	0.3277	0.4119	1.04E-02	1.05E-20
1	0.2251	0.5076	0.4742	1.81E-02	7.09E-21
1.25	0.1626	0.7172	0.5049	2.80E-02	4.86E-21
1.5	0.1023	0.9494	0.5111	3.95E-02	3.37E-21
1.75	4.40E-02	1.198	0.4996	5.24E-02	2.35E-21
2	-1.26E-02	1.458	0.4757	6.63E-02	1.65E-21
2.25	-6.80E-02	1.726	0.4436	8.08E-02	1.16E-21
2.5	-0.1223	1.998	0.4066	9.58E-02	8.18E-22
2.75	-0.1759	2.272	0.3673	0.1112	5.76E-22
3	-0.2287	2.546	0.3276	0.1268	4.04E-22
3.25	-0.281	2.819	0.2888	0.1426	2.83E-22
3.5	-0.3327	3.089	0.252	0.1587	1.97E-22
3.75	-0.3838	3.357	0.2181	0.1751	1.37E-22
4	-0.4343	3.621	0.1873	0.1918	9.53E-23
4.25	-0.4841	3.881	0.16	0.2089	6.61E-23
4.5	-0.5331	4.138	0.1361	0.2264	4.59E-23
4.75	-0.5813	4.39	0.1155	0.2444	3.19E-23
5	-0.6285	4.639	9.79E-02	0.2629	2.22E-23
5.25	-0.6746	4.885	8.31E-02	0.282	1.55E-23
5.5	-0.7195	5.128	7.06E-02	0.3015	1.09E-23
5.75	-0.7632	5.368	6.03E-02	0.3217	7.72E-24
6	-0.8055	5.606	5.18E-02	0.3424	5.50E-24
6.25	-0.8463	5.842	4.48E-02	0.3636	3.96E-24
6.5	-0.8856	6.076	3.90E-02	0.3854	2.87E-24
6.75	-0.9233	6.308	3.43E-02	0.4077	2.10E-24
7	-0.9594	6.539	3.05E-02	0.4306	1.56E-24
7.25	-0.9937	6.769	2.74E-02	0.454	1.17E-24
7.5	-1.026	6.997	2.49E-02	0.4778	8.87E-25
7.75	-1.057	7.225	2.30E-02	0.5022	6.81E-25
8	-1.086	7.451	2.15E-02	0.527	5.30E-25

J. Jones
Staylor

N. Sridhar

9/18/98

Syn J13 Water evaporation. at higher temp.

① 160g. using OLI (OLI Esp 6.2e)

Note OLI only good for $T_{mo} > 6.5$

$0 < T < 30$.

The following calculation may not be valid

Syn_J13_Evap_160.xls Summary_sheet Page 1 12/8/00

	input 25oC	Amount lost during evapor.	Amount left after evap	C of liquid after evap at 160oC	C of liquid if analyzed at 25oC
	mg/L	mg	mg	mg/L	mg/L
Ca	7.446	6.0852	1.3608	1.34E+02	1.02E+03
Cl	6.9	685.68428	-678.7843	-6.69E+04	-5.09E+05
F	2.2	9.2587004	-7.0587	-6.96E+02	-5.30E+03
HCO3	100	7500.2245	-7400.225	-7.30E+05	-5.55E+06
K	6.16657	221.94705	-215.7805	-2.13E+04	-1.62E+05
Mg	2.5597	0	2.5597	2.52E+02	1.92E+03
Na	53.5215	4004.3069	-3950.785	-3.90E+05	-2.96E+06
NO3	46	0.0001035	45.9999	4.54E+03	3.45E+04
SO4	18.1	1808.1024	-1790.002	-1.76E+05	-1.34E+06
Si	11.3	6.2275824	5.072418	5.00E+02	3.81E+03
pH	7.98174			10.3622	10.0623
Sum (mg/L)	2.54E+02			-1.38E+06	-1.05E+07
Density (kg/m^3)	1.008353			0.2412601	1.8358794
Volume of liquid (m^3/hr or m^3)				1.01E-05	1.33E-06

Note: pH= 8.205 (Before SiO2 introduced)

J. Jones
3/1/00

Results are negative. This back subtraction method may not work. However look page 37 and 38. There is still water and conductivity still high.

Syn_J13_Evap_160.xls Data_sheet Page 1/2 12/8/00

Stream	Table16	V_Syn_J13	L_Syn_J13	S_Syn_J13	Out	Species	FW	amount to vapour mole	amount to Solid mole	Total lost in Evapora mg
Phase	Mixed	Vapor	Aqueous	Solid	Mixed					
Temperature, C	25	160	160	160	25					
Pressure, atm	1	1	1	1	1					
pH	7.98174		10.3622		10.0623					
Total mol/hr	55.8597	55.7517	0.0566408	9.99E-02	0.0567026					
Flow Units	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr					
H2O	55.6955	55.69	0.0301065		0.0301645	Ca	40		1.52E-04	6.0852
H2F2	5.11E-03	1.18E-11	5.62E-05			CL	35.5	1.10E-10	1.93E-02	685.684279
CO2	3.69E-02		1.87E-10		1.86E-10	F	19	1.83E-04	3.04E-04	9.25870045
H2SO4						HCO3	61		6.14E-02	7500.2245
HCL	0.0208575	1.10E-10			8.66E-06	K	39		0.005691	221.94705
HF	1.19E-07	1.83E-04			4.30E-14	Mg	24.3		0.00E+00	0
HNO3	1.38E-02	1.67E-09	1.45E-11		4.0901E-16	Na	23		0.1741003	4004.3069
SICL4	9.0522E-06					NO3	62	1.67E-09		0.00010345
SIF4		4.1229E-16				SO4	96		0.0188344	1808.1024
SO3						Si	28.1		0.0002218	6.2275824
H2SIO3	2.04E-04		1.68E-08		1.92E-07					
KCL	1.14E-06		1.58E-03	0.00569095	9.84E-04					
KHSO4	6.8059E-13		7.78E-17							
MGCO3										
MGH2SIO4										
MGSO4										
NAF	7.16E-04		8.23E-03	0	1.07E-02					
NAHCO3	4.31E-03		8.21E-06		2.85E-06					
NAHSIO3	4.48E-05		1.89E-04		2.34E-04					
NANO3	2.25E-05		9.79E-03		6.63E-03					
CASO4	2.16E-07				3.44E-16					
CAH2SIO4	5.21E-13			0	5.42E-16					
SIO2	2.05E-04		1.22E-06	0.00022178	6.88E-06					
CACO3	3.30E-07		8.46E-16	0.00E+00	6.72E-14					
H2CO3										
H6F6										
KMGCL3										
KOH			0.0000529							
NA3HSO42				0						
NA6SO42CO3	9.47E-03		5.01E-05	0	2.04E-05					
MGOH2				0.00E+00						
NAOH					4.76E-07					
CAOH2										
CA2CL2O.2H2O										
CACL2.1H2O										
CACL2.2H2O										
CACL2.4H2O										
CACL2.6H2O										
CACL2					1.12E-13					
CAF2	0.00014938			1.52E-04						
CANO32.3H2O										
CANO32.4H2O										
CANO32	2.20E-06		1.7957E-13							
CASO4.2H2O				0						
K2CO3.1.5H2O										
K2CO3	6.95E-03		0.000048596							
K2SO4.1H2O										
K2SO4										

J. Jones
3/1/00

Aqueous.

K3NASO42				
KF.2H2O				
KF.4H2O				
KF	0.0024061			
KHCO3				
KMGCL3.2H2O				
KNO3	0.00407775		0.00722989	
KOH.1H2O				
KOH.2H2O				
MGCL2.2H2O				
MGCL2.4H2O				
MGCL2.6H2O				
MGCL2				
MGCLOH				
MGCO3.3H2O				
MGF2		0		
MGNO32.2H2O				
MGNO32.6H2O				
MGNO32				
MGSO4.1H2O				
MGSO4.6H2O				
MGSO4.7H2O				
MGSO4OH.0.5H2O				
MGSO4OH				
NA2CO3.10H2O				
NA2CO3.1H2O		0		
NA2CO3.7H2O				
NA2CO3	6.54E-02		0.0614037	8.37E-05
NA2SIO3.5H2O				
NA2SIO3.6H2O				
NA2SIO3.9H2O				
NA2SIO3	5.13E-05			4.68E-07
NA2SO4.10H2O				
NA2SO4			0.0188344	
NA3FSO4				5.94E-05
NACL			0.0136241	5.87E-04
NAHF2			0	
NAHSO4				
NAOH.1H2O				
Total g/hr	1018.86	1005.98	2.44686	10.4291 2.44686
Volume, m3/hr	0.00101042	1.97066	1.01E-05	4.16E-06 1.33E-06
Enthalpy, cal/hr	-3.84E+06	-3.16E+06	-5264.61	-24483.1 -5409.63
Vapor fraction		1		
Solid fraction	2.6742E-06		1	3.42E-01
Organic fraction				
Osmotic Pres, atm	8.1305		464.935	623.402
Redox Pot, volts				
E-Con, 1/ohm-cm	1.59E-02		0.490378	0.241999
E-Con, cm2/ohm-mol	51.7807		30.2837	7.02455
Abs Visc, cP	0.951581		20165.7	3.43607
Rel Visc	1.06833		118360	3.85764
Ionic Strength	0.21882		33.8754	13.0215

J. Jones
2/1/02

Water 0.0301' mol/hr = 0.5418
Total total 2.44 g/hr

$$\text{wt \%} = \frac{0.5418}{2.44} = 22.2\% \text{ in the aqueous phase}$$

This number may not be correct, because OLI
d.y. 12/08/00.
does not work at $x_{\text{H}_2\text{O}} \leq 0.6$.

Does DOE have real measurement on
the wt% — temperature relationship

d.y. 12/08/00
may be hard to measure. Perhaps use
conductivity probe.

A review of past data showed.

	Total mol/hr	H ₂ O mol/hr	Total g/hr	E. cond. 1/ohm-cm	I
Syn J13-Evap-120	0.0036033	0.0036033	0.188176	0.6407	0.72 16.9
Syn-J13-Evap-108	0.01214	0.0108865	0.3498	0.5439	0.86 9.608
Syn-J13-Evap-104	0.02500	0.02327	0.603	0.3039	0.86 3.925
Syn-J13-Evap-101	0.1010	0.09928	1.470	0.460	6.17
Syn-J13-Evap-160	0.07664	0.03010	2.446	0.2114	1.465
Syn-J13-Evap-160	0.07664	0.03010	2.446	0.4403	0.531 33.37

J. Jones
2/1/02

Jan. 26/01

Vapor pressure of saturated salts. using OLI Exp 6.2

① NaCl, $KNO_3 + NaNO_3$ (16.39°C) (289.39°K)

$$P_{H_2O} = 0.1216 \text{ atm (see page 42)}$$

$$P_{H_2O}^{\circ}(29^{\circ}K) = 0.01917 \text{ Bar. (Handbook value)}$$

$$P_{H_2O}^{\circ}(t=16.39) = 0.018473 \text{ atm (OLI), close Handbook value.}$$

$$\text{so Rel. Hum.} = \frac{0.1216}{0.018473} = 0.658\%$$

Note: Hand book value: CRC, 54th edition Page 46:

$$\text{Rel. Hum} = 30.49\%$$

② Pure water.

$$P_{H_2O}(16.39^{\circ}C) = 0.018473 \text{ atm.}$$

③ KCl pure salt

$$P_{H_2O} = 0.0158259 \text{ atm, } RH = \frac{0.0158259}{0.018473} = 0.8566$$

④ NaCl simple salt

$$P_{H_2O} = 0.0139816 \text{ atm, } RH = \frac{0.01398}{0.01847} = 0.7569$$

↑
RH
7/14/02

↑
RH
2/14/02

ESP V-6.2

PROCESS:EVAP_CTP

01/26/2001 PAGE 5

STREAM: Solid
TO :
FROM : NaKClNO3

① NaCl, H₂O₃

+ NaOH

Phases----->	Aqueous	Solid	Vapor	Organic
Temperature, C	16.39	16.39	16.39	16.39
Pressure, atm	0.0121635	0.0121635	0.0121635	0.0121635
pH	0.0			
Total mol/hr	0.0	6.99772	0.0	0.0
	mol/hr-----	mol/hr-----	mol/hr-----	mol/hr-----
H2O	0.0	0.0	0.0	0.0
H2	0.0	0.0	0.0	0.0
HCL	0.0	0.0	0.0	0.0
HNO3	0.0	0.0	0.0	0.0
O2	0.0	0.0	0.0	0.0
NANO3	0.0	1.95626	0.0	0.0
KCL	0.0	0.0	0.0	0.0
NACL	0.0	2.2946	0.0	0.0
KNO3	0.0	2.74686	0.0	0.0
KOH.1H2O	0.0	0.0	0.0	0.0
KOH.2H2O	0.0	0.0	0.0	0.0
KOH	0.0	0.0	0.0	0.0
NAOH.1H2O	0.0	0.0	0.0	0.0
NAOH	0.0	0.0	0.0	0.0
=====				
Total g/hr	0.0	578.092	0.0	0.0
Volume, m3/hr	0.0	2.6734E-04	0.0	0.0
Enthalpy, cal/hr	0.0	-7.6968E+05	0.0	0.0
Density, g/m3		2.1624E+06		
Vapor fraction	0.0	0.0	0.0	0.0
Solid fraction	0.0	1.	0.0	0.0
Organic fraction	0.0	0.0	0.0	0.0
Osmotic Pres, atm	0.0			
Redox Pot, volts	0.0			
E-Con, 1/ohm-cm	0.0			
E-Con, cm2/ohm-mol	0.0			
Abs Visc, cP	0.0			
Rel Visc	0.0			
Ionic Strength	0.0			

$P_{mix} = 0.01216$

$RH = \frac{0.01216}{0.018473} = 0.658$

See ②

Hand book = 30.44 %

of vapor 2/1/02

⑤

NaNO3, 16.39°C

$P = 0.0136496 \text{ atm}, RH = \frac{0.0136496}{0.018473} = 0.739\%$

⑥

KNO3, 16.39°C

$P = 0.0173728 \text{ atm}, RH = \frac{0.01737}{0.018473} = 0.9405\%$

Therefore, all P of simple salts are higher than their mixed salt. Both from handbook and from OLI simulation.

At 60°C

⑦

KNO3 solid, 60°C

$P_{mix} = 0.1707 \text{ atm}, RH = \frac{0.1707}{0.1965} = 0.866\%$

* 0.19695 atm is for pure water obtained using OLI.

Note that Handbook value is 82%, see handbook (page 41).

⑧

pure water $P^0 = 0.4673 \text{ atm}, T = 80^\circ\text{C}$

⑨

pure water $P^0 = 0.19695 \text{ atm}, T = 60^\circ\text{C}$

of vapor 3/1/02

(10): NaN03 at 30°C
 $P = 0.26463$; $RH = \frac{0.26463}{0.4673} = 0.567$
 close to hand book value, 65.6% (CRC book, Page 41) ^{see} Notebook.

(11) NaCl at 30°C
 $P = 0.3487$; $RH = \frac{0.3487}{0.4673} = 0.7462$
 Handbook value = 76.4% (CRC book, see page 41 of Notebook)

(12) Input 4 salts, sometimes get two solid
 See page 45.

*Input
 3/14/02*

ESP V-6.2

PROCESS:EVAP_CTP

01/26/2001 PAGE 5

(12)

Input 4 species.
NaCl + NaNO₃ + HNO₃ + H₂O

STREAM: Solid
 TO :
 FROM : NaKClNO3

Phases----->	Aqueous	Solid	Vapor	Organic
Temperature, C	16.39	16.39	16.39	16.39
Pressure, atm	0.0129979	0.0129979	0.0129979	0.0129979
pH	0.0			
Total mol/hr	0.0	22.4145	0.0	0.0
-----	mol/hr-----	mol/hr-----	mol/hr-----	mol/hr-----
H2O	0.0	0.0	0.0	0.0
H2	0.0	0.0	0.0	0.0
HCL	0.0	0.0	0.0	0.0
HNO3	0.0	0.0	0.0	0.0
O2	0.0	0.0	0.0	0.0
NANO3	0.0	0.0	0.0	0.0
KCL	0.0	0.0	0.0	0.0
NACL	0.0	10.4796	0.0	0.0
KNO3	0.0	11.9349	0.0	0.0
KOH.1H2O	0.0	0.0	0.0	0.0
KOH.2H2O	0.0	0.0	0.0	0.0
KOH	0.0	0.0	0.0	0.0
NAOH.1H2O	0.0	0.0	0.0	0.0
NAOH	0.0	0.0	0.0	0.0
-----	-----	-----	-----	-----
Total g/hr	0.0	1819.11	0.0	0.0
Volume, m3/hr	0.0	8.5521E-04	0.0	0.0
Enthalpy, cal/hr	0.0	-2.4426E+06	0.0	0.0
Density, g/m3		2.1271E+06		
Vapor fraction	0.0	0.0	0.0	0.0
Solid fraction	0.0	1.	0.0	0.0
Organic fraction	0.0	0.0	0.0	0.0
Osmotic Pres, atm	0.0			
Redox Pot, volts	0.0			
E-Con, 1/ohm-cm	0.0			
E-Con, cm2/ohm-mol	0.0			
Abs Visc, cP	0.0			
Rel Visc	0.0			
Ionic Strength	0.0			

end up

*Input
 3/14/02*

Solubility Calculations

① NaF at 100°C

using Esp V-6.2

$$\text{Volume} = 0.104895 \times 10 \text{ L}$$

$$F(\text{NaF}) = 1.19357 \text{ mol/hr}$$

$$F(\text{H}_2\text{O}) = 55.5 \text{ mol/hr}$$

$$\text{Solubility} = \frac{1.193}{\frac{55.5}{1000} \times 18} = 1.19 \text{ molal}$$

See attached sheet on Page 47

J. J. J.
2/10/02

STREAM: L
TO :
FROM : Sept
print out for liquid stream of separator

Solubility
① NaF

Phases	Aqueous	Solid	Vapor	Organic
Temperature, C	100.	100.	100.	100.
Pressure, atm	1.	1.	1.	1.
pH	7.86975			
Total mol/hr	56.6932	0.0	0.0	0.0

	mol/hr	mol/hr	mol/hr	mol/hr
H2O	55.5	0.0	0.0	0.0
H2F2	5.9887E-13	0.0	0.0	0.0
CO2	0.0	0.0	0.0	0.0
H2SO4	0.0	0.0	0.0	0.0
HF	4.0722E-05	0.0	0.0	0.0
HNO3	0.0	0.0	0.0	0.0
SO3	0.0	0.0	0.0	0.0
NAF	1.19307	0.0	0.0	0.0
NAHCO3	0.0	0.0	0.0	0.0
NANO3	0.0	0.0	0.0	0.0
KHSO4	0.0	0.0	0.0	0.0
KNO3	0.0	0.0	0.0	0.0
K2SO4	0.0	0.0	0.0	0.0
NA2SO4	0.0	0.0	0.0	0.0
KF	0.0	0.0	0.0	0.0
K2CO3	0.0	0.0	0.0	0.0
NA2CO3	0.0	0.0	0.0	0.0
K2CO3.1.5H2O	0.0	0.0	0.0	0.0
K2SO4.1H2O	0.0	0.0	0.0	0.0
K3NASO42	0.0	0.0	0.0	0.0
KF.2H2O	0.0	0.0	0.0	0.0
KF.4H2O	0.0	0.0	0.0	0.0
KHCO3	0.0	0.0	0.0	0.0
KOH.1H2O	0.0	0.0	0.0	0.0
KOH.2H2O	0.0	0.0	0.0	0.0
KOH	0.0	0.0	0.0	0.0
NA2CO3.10H2O	0.0	0.0	0.0	0.0
NA2CO3.1H2O	0.0	0.0	0.0	0.0
NA2CO3.7H2O	0.0	0.0	0.0	0.0
NA2SO4.10H2O	0.0	0.0	0.0	0.0
NA3FSO4	0.0	0.0	0.0	0.0
NA3HSO42	0.0	0.0	0.0	0.0
NA6SO42CO3	0.0	0.0	0.0	0.0
NAHF2	0.0	0.0	0.0	0.0
NAHSO4	0.0	0.0	0.0	0.0
NAOH.1H2O	0.0	0.0	0.0	0.0
NAOH	4.0722E-05	0.0	0.0	0.0
H2CO3	0.0	0.0	0.0	0.0
H6F6	0.0	0.0	0.0	0.0
=====				
Total g/hr	1049.95	0.0	0.0	0.0
Volume, m3/hr	0.00104895	0.0	0.0	0.0
Enthalpy, cal/hr	-3.8804E+06	0.0	0.0	0.0
Density, g/m3	1.0010E+06			
Vapor fraction	0.0	0.0	0.0	0.0
Solid fraction	0.0	0.0	0.0	0.0
Organic fraction	0.0	0.0	0.0	0.0
Osmotic Pres, atm	58.9172			
Redox Pot, volts	0.0			
E-Con, 1/ohm-cm	0.178208			
E-Con, cm2/ohm-mol	93.4643			
Abs Visc, cP	0.400901			

$$\frac{1.193}{\frac{104895}{1000}} = 1.137 \text{ molal}$$

$$\frac{1.193}{\frac{55.5}{1000} \times 18} = 1.19 \text{ molal}$$

$$I = 0.48$$

on page 4,
Print out for
Solid stream
shown 0.30689
of NaF.

J. J. J. 1/31/01
Page 4 of
the print out
is not included
in the notebook.
J. J. J. 1/31/01

J. J. J.
2/10/02

② solubility of K_2SO_4 , $100^\circ C$.

$$S = \frac{1.1329 \text{ mol/hr}}{\frac{48 \times 18}{1000}} = 1.34 \text{ molal}$$

$$I (\text{strength}) = 2.76$$

③ KNO_3 , $100^\circ C$

$$S = \frac{9.033 \text{ mol/hr}}{\frac{20 \times 18}{1000}} = 25.09 \text{ molal}$$

$$I = \frac{0.966}{25.07} \quad \text{J.Y. 1/31/01}$$

$$\text{Water Fraction} = \frac{20}{29.033} = 0.68887$$

This \rightarrow within OLI limit.

④ Solubility of $NaNO_3$ at $100^\circ C$

$$S = \frac{7.685 \text{ mol/hr}}{\frac{20 \times 18}{1000}} = 21.3 \text{ molal}$$

$$I = 21.178$$

$$X_{H_2O} = \frac{20}{27.6857} = 0.722$$

o.k.

J.Y.
skator

Note: the results are not printed. It is easy to do the calculation with OLI.

Stream Analyzer version 1.01 is

a new release of the OLI software.

It is window based - it is very user friendly.

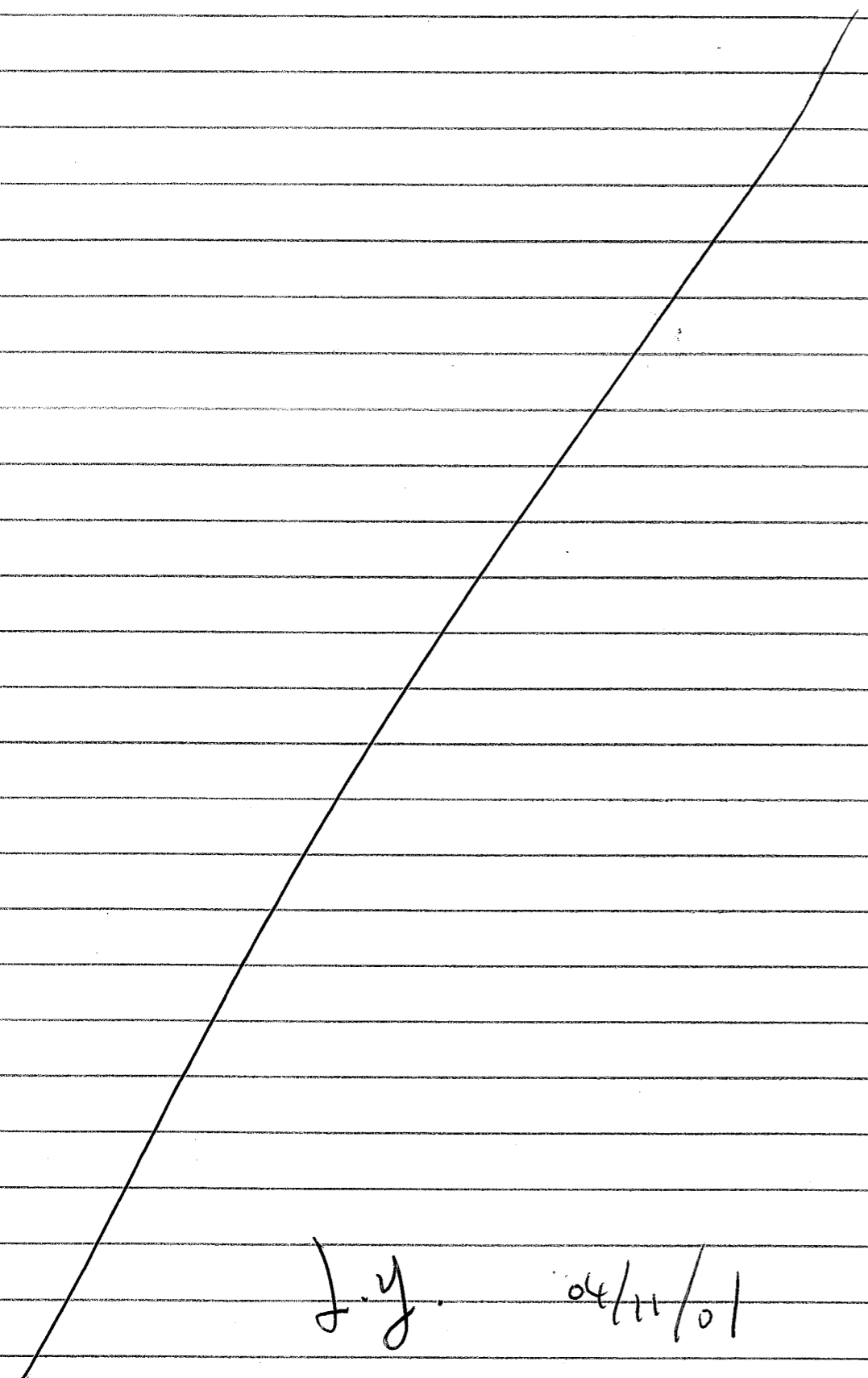
Due to the approaching release date of

another version of the software, QA paper work will be done after the new release is received.

The results obtained with Stream Analyzer

should only be used as non-decision making information only.

J.Y. April 12/01



J. Y. 04/11/01

Calculate the water activity at 25°C for NaCl + NaNO₃ system.

(0.1 mol)

Do equilibrium calculation given vapour amount, giving temperature (25°C). The software calculate the water activity, vapour pressure of salt solution. The results are as follows (Note print out not attached, The result can be easily obtained in a second if give the input (The results from one run are given in pages 52, 53, 54)

[NaCl_NaNO3_Activity.xls

[Date]

J. Y. 02/12/01

OLI_Simulation_Results

T=25 oC

Run#	Input			liquid				Output					
	Water	NaCl	NaNO ₃	Water	NaCl	NaNO ₃	x(Water)	I	NaCl	NaNO ₃	Vapour Water	P(H ₂ O)	a(H ₂ O)
1	55.508	10	10	55.408	3.716	6.8202	0.840226	10.46	6.284	3.1798	0.1	0.020865	0.66491
2	55.508	8	10	55.408	3.716	6.8202	0.840226	10.46	4.284	3.1798	0.1	0.020865	0.66491
3	55.508	3.8	10	55.408	3.716	6.8202	0.840226	10.46	0.084	3.1798	0.1	0.020865	0.66491
4	55.508	3.8	6.83	55.408	3.716	6.8202	0.840226	10.46	0.084	0.0098	0.1	0.020865	0.66491
5	55.508	3	6.8	55.408	3	6.8	0.849712	9.7522	0	0	0.1	0.021767	0.69365
In the above, the both solid salts are present, the solution composition are the same (Eutonic), water activity are the same above not saturated													
6	55.508	3	12	55.408	3	7.5103	0.840556	10.425	0	4.4897	0.1	0.021237	0.67677
7	55.508	3	7.6	55.408	3	7.5103	0.840556	10.425	0	0.0897	0.1	0.021237	0.67677
8	55.508	2	12	55.408	2	8.5509	0.840038	10.452	0	3.4491	0.1	0.021707	0.69175
9	55.508	0	12	55.408	0	10.888	0.835767	10.761	0	1.112	0.1	0.022251	0.71717
10	55.508	0.1	12	55.408	0.1	10.763	0.836082	10.738	0	1.237	0.1	0.022469	0.71602
11	55.508	0.5	12	55.408	0.5	10.273	0.837219	10.653	0	1.727	0.1	0.02232	0.71129
12	55.508	1	12	55.408	1	9.6781	0.838421	10.565	0	2.3219	0.1	0.022127	0.70512
13	55.508	1.5	12	55.408	1.5	9.1039	0.839364	10.498	0	2.8961	0.1	0.021923	0.69862
The above shows the solubility of NaNO ₃ and the activity of water as a function of NaCl													
14	55.508	10	0	55.408	6.14	0	0.90024	6.1511	3.86	0	0.1	0.023744	0.75662
15	55.508	10	0.1	55.408	6.0983	0.1	0.899389	6.2082	3.9017	0	0.1	0.023699	0.7552
16	55.508	6.1	0.1	55.408	6.0983	0.1	0.899389	6.2082	0.0017	0	0.1	0.023699	0.7552
17	55.508	10	0.5	55.408	5.9336	0.5	0.895966	6.4381	4.0664	0	0.1	0.023521	0.74954
18	55.508	10	1	55.408	5.7319	1	0.891665	6.7297	4.2681	0	0.1	0.023301	0.74253
19	55.508	10	2	55.408	5.3423	2	0.882992	7.3269	4.6577	0	0.1	0.022868	0.72872
20	55.508	10	4	55.408	4.6177	4	0.865402	8.576	5.3823	0	0.1	0.022022	0.70179
21	55.508	10	5	55.408	4.2821	5	0.856514	9.2277	5.7179	0	0.1	0.021608	0.6886
22	55.508	10	6	55.408	3.964	6	0.84758	9.8972	6.036	0	0.1	0.021198	0.67555
23	55.508	10	6.5	55.408	3.8114	6.5	0.8431	10.239	6.1886	0	0.1	0.020995	0.66906
24	55.508	10	6.8	55.408	3.722	6.8	0.840406	10.446	6.278	0	0.1	0.020873	0.66518
25	55.508	10	7	55.408	3.716	6.8202	0.840226	10.46	6.284	0.1798	0.1	0.020865	0.66491
26	55.508	10	17	55.408	3.716	6.8202	0.840226	10.46	6.284	10.1798	0.1	0.020865	0.66491
The above shows the solubility of NaCl and the activity of water as a function of NaNO ₃													
27	55.508	0	0	55.408	0	0	1.00E-07	0	0	0	0.1	0.031385	1

Numbers in the table are in Moles
I and x(water) are all within the limits (30, 0.65)

Calculation Summary

Run #1

SinglePoint1 Calculation for Stream1

Automatic Chemistry Model
Public Databank

Vapor Amount Calculation

oil mol in vapour.

Temperature 25.000 C
Pressure 0.020865 atm

Stream Parameters

Stream Amount 75.508 mol
Temperature 25.000 C
Pressure 0.020865 atm
pH 6.9902
Osmotic Pressure 582.32 atm
Ionic Strength 10.460 mol/kg H2O
WaterActivity 0.66491 Activity
Electrical Cond, specific 0.23231 1/Ohm
Electrical Cond, molar 15.213 cm2/ohm-mol
Viscosity, absolute 2.6681 cP
Viscosity, relative 2.9955 cP/cP H2O

	Units	Total	Aqueous	Vapor	Solid	Organic
Density	g/ml	n/a	1.3706	1.5368e-5	2.2023	0.0
Enthalpy	cal	-5.8522e6	-4.8733e6	-5779.8	-9.7312e5	0.0

Stream Inflows

Water Input 55.508 mol
Sodium chloride Input 10.0000 mol Final 10.000 mol
Sodium nitrate Input 10.000 mol

Scaling Tendencies

solids within temperature range
Sodium nitrate 1.0000
Sodium chloride 1.0000
Sodium hydroxide monohydrate 1.2129e-11

Total and Phase Flows

	Units	Total	Aqueous	Vapor	Solid	Organic
Molar flow	mol	75.508	76.385	0.100000	9.4638	0.0
Mass flow	g	2434.4	1795.0	1.8015	637.52	0.0
Volumetric flow	L	118.82	1.3097	117.22	0.28948	0.0

Species Output

	Total	Aqueous	Vapor	Solid	Organic
	mol	mol	mol	mol	n/a
H2O	55.508	55.408	0.100000	0.0	0.0
NaCl	6.2840	0.0	0.0	6.2840	0.0
NaNO3	3.2753	0.095508	0.0	3.1798	0.0
HCl	1.8997e-12	1.0306e-13	1.7967e-12	0.0	0.0
HNO3	9.0409e-10	9.0104e-10	3.0480e-12	0.0	0.0
H+1	2.0482e-8	2.0482e-8	0.0	0.0	0.0
OH-1	2.1388e-8	2.1388e-8	0.0	0.0	0.0
Na+1	10.441	10.441	0.0	0.0	0.0
Cl-1	3.7160	3.7160	0.0	0.0	0.0
NO3-1	6.7248	6.7248	0.0	0.0	0.0

Molecular Output

solubility

	Total	Aqueous	Vapor	Solid	Organic
	mol	mol	mol	mol	n/a
H2O	55.508	55.408	0.100000	0.0	0.0
NaCl	10.000	3.7160	0.0	6.2840	0.0
NaNO3	10.000	6.8202	0.0	3.1798	0.0
HCl	1.8997e-12	1.0306e-13	1.7967e-12	0.0	0.0
NaOH	9.0598e-10	9.0598e-10	0.0	0.0	0.0
HNO3	9.0408e-10	9.0104e-10	3.0480e-12	0.0	0.0

Elements

	Aqueous	Vapor	Solid	Organic
	mol	mol	mol	n/a
CL(-1)	3.7160	1.7967e-12	6.2840	0.0
H(+1)	110.82	0.20000	0.0	0.0
N(+5)	6.8203	3.0480e-12	3.1798	0.0
NA(+1)	10.536	0.0	9.4638	0.0
O(-2)	75.869	0.10000	9.5394	0.0

Speciation Summary

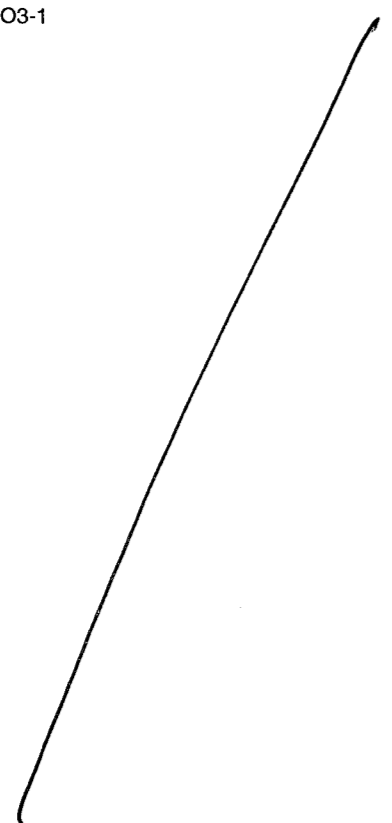
2-y.
02/12/01

SinglePoint1 Results
2/9/01 3:21:03 PM

StreamAnalyzer

Page 3 of 3
OLI Systems, Inc.

User Inflows	Related Inflows	Aqueous Species	Vapor Species	Solid Species	Organic Species
H2O	NaOH.1H2O	H2O	H2O - Vap	NaOH.1H2O	
NaCl	HCl	HCl - Aq	HCl - Vap	NaCl - Solid	
NaNO3	NaOH	NaNO3 - Aq	HNO3 - Vap	NaOH - Solid	
	HNO3	HNO3 - Aq		NaNO3 - Solid	
		H+1			
		OH-1			
		Na+1			
		Cl-1			
		NO3-1			



L.y. *02/12/01*

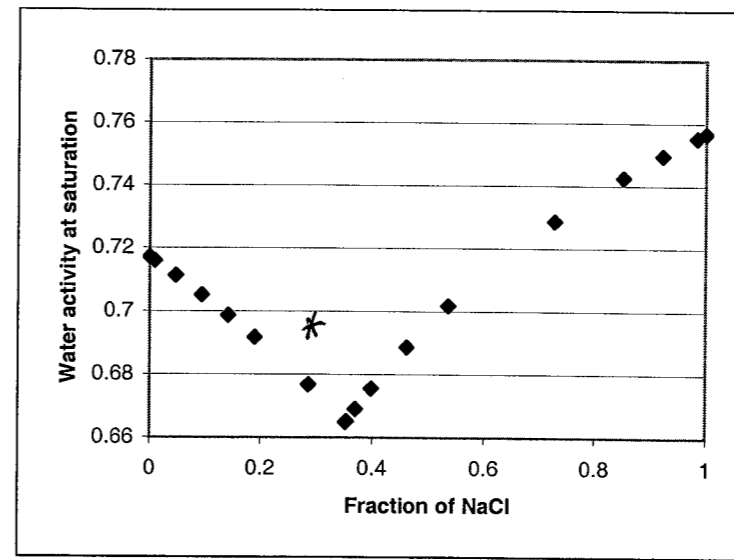
NaCl_NaNO3_Activity.xls

2/12/01

Water_Activity_at_Saturation

T=25 oC

Simulation	Water	NaCl	NaNO3	Fraction	Activity
1	55.408	3.716	6.8202	0.352689	0.66491
2	55.408	3.716	6.8202	0.352689	0.66491
3	55.408	3.716	6.8202	0.352689	0.66491
4	55.408	3.716	6.8202	0.352689	0.66491
5	This run is non saturated				
6	55.408	3	7.5103	0.285434	0.67677
7	55.408	3	7.5103	0.285434	0.67677
8	55.408	2	8.5509	0.189557	0.69175
9	55.408	0	10.888	0	0.71717
10	55.408	0.1	10.763	0.009206	0.71602
11	55.408	0.5	10.273	0.046412	0.71129
12	55.408	1	9.6781	0.09365	0.70512
13	55.408	1.5	9.1039	0.141457	0.69862
14	55.408	6.14	0	1	0.75662
15	55.408	6.0983	0.1	0.983867	0.7552
16	55.408	6.0983	0.1	0.983867	0.7552
17	55.408	5.9336	0.5	0.922283	0.74954
18	55.408	5.7319	1	0.851454	0.74253
19	55.408	5.3423	2	0.727606	0.72872
20	55.408	4.6177	4	0.535839	0.70179
21	55.408	4.2821	5	0.461329	0.6886
22	55.408	3.964	6	0.397832	0.67555
23	55.408	3.8114	6.5	0.36963	0.66906
24	55.408	3.722	6.8	0.353735	0.66518
25	55.408	3.716	6.8202	0.352689	0.66491
26	55.408	3.716	6.8202	0.352689	0.66491



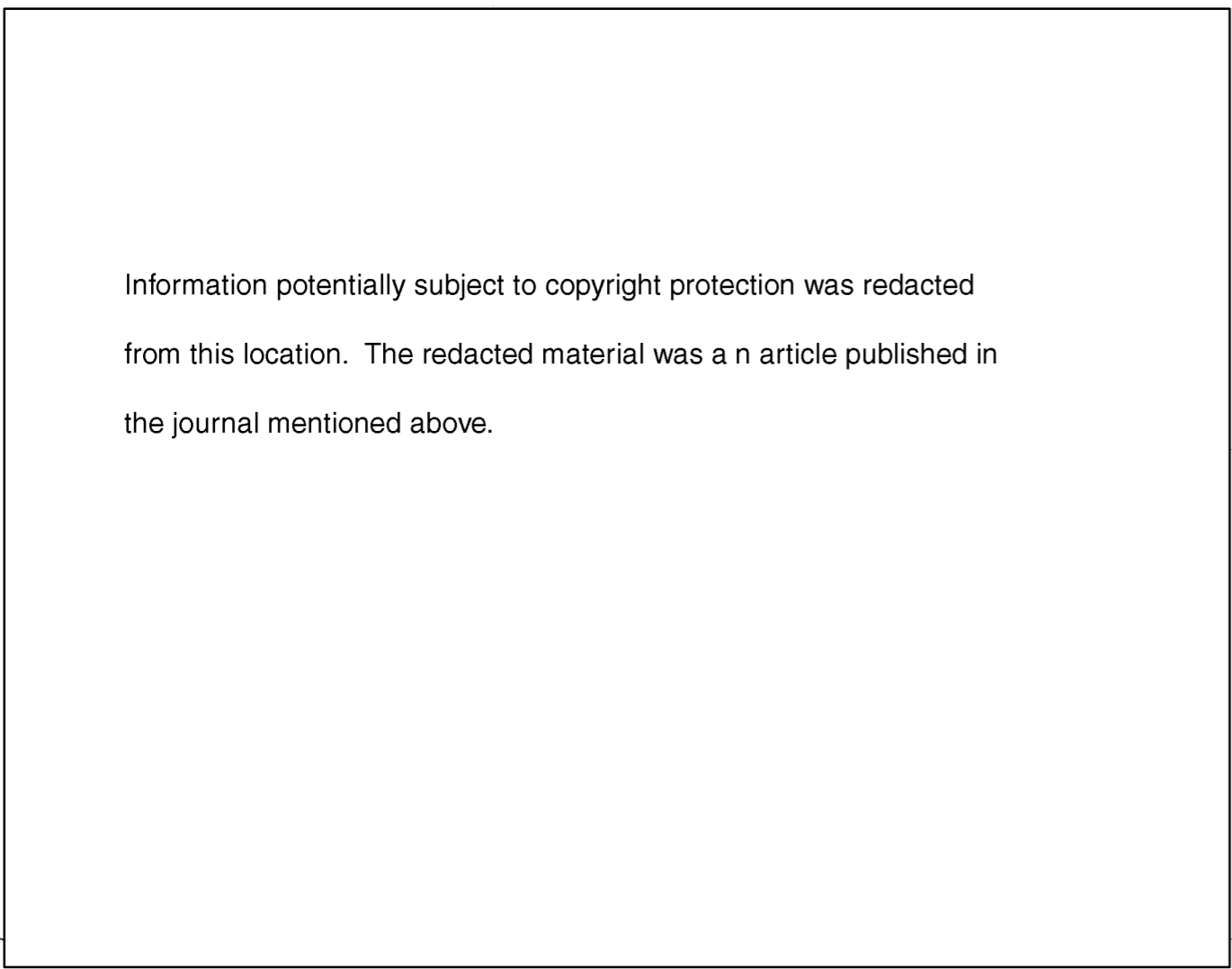
L.y.
02/12/01

very close to published results. see page 56.

** would be for run 5.*

176 J. Phys. Chem. A, Vol. 102, No. 1, 1998

Ge et al.



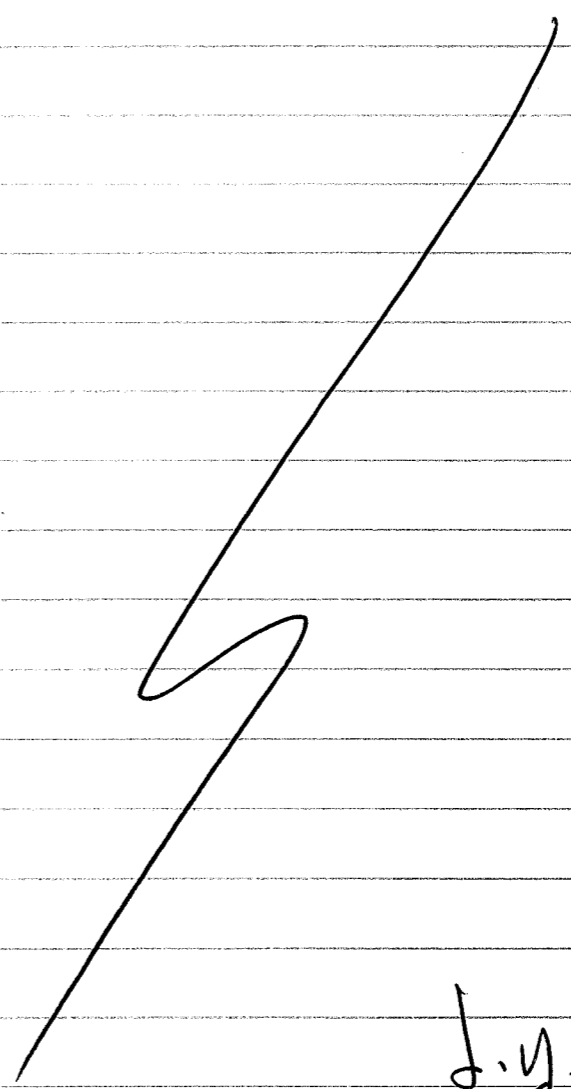
published Results.

J.y. 02/12/01

Comparison of OLI Results with Published Results

This work is postponed until a full release of OLI StreamAnalyzer is received.

J.y. 04/11/01



J.y. 04/11/01

Calculation of the Chemistry Lead containing salts using OLI ESP 6.2e
April 11, 2001

The objective is to know the speciations of of lead in NaCl, LiCl solutions at 80, 100, and 120 °C. The background is given in the e-mail attached:

100 J. Yang
03/31/06

J. Yang
04/10/01

-----Original Message-----

From: Gustavo Cragnolino [mailto:gcragnolino@gargol.cnwra.swri.edu]

Sent: Monday, April 09, 2001 8:42 AM

To: nsridhar@gargol.cnwra.swri.edu; ddunn@gargol.cnwra.swri.edu; 'Vijay Jain (vjain)'; 'Gustavo Cragnolino'; 'Yi-ming Pan (ypan)'; 'Sean Brossia (sbrossia)'; 'Lietai Yang'

Subject: RE: Augmented work

I agree with Sridhar. Let's do NaCl with the test matrix Darrell suggested and later decide depending upon the results. Rather than go the LiCl route I prefer to evaluate the overall set of anions and evaluate other potential detrimental cations within ranges of concentrations that are achievable.

-----Original Message-----

From: Narasi Sridhar [mailto:nsridhar@gargol.cnwra.swri.edu]

Sent: Friday, April 06, 2001 4:58 PM

To: ddunn@gargol.cnwra.swri.edu; 'Vijay Jain (vjain)'; 'Gustavo Cragnolino'; 'Yi-ming Pan (ypan)'; 'Sean Brossia (sbrossia)'; 'Lietai Yang'

Subject: RE: Augmented work

I don't think we should go the route of Catholic in terms of using HCl. I think this is unrealistic and we would be subject to the same criticisms that they have been. I would lean towards using NaCl solutions with lead chloride. But maybe Lietai can do different simulations and find

J. Yang
7/10/02

out what is best.

-----Original Message-----

From: Darrell Dunn [mailto:ddunn@gargol.cnwra.swri.edu]

Sent: Friday, April 06, 2001 4:48 PM

To: Vijay Jain (vjain); Gustavo Cragnolino; Yi-ming Pan (ypan); Narasi Sridhar (nsridhar); Sean Brossia (sbrossia); Lietai Yang

Subject: Augmented work

Augmented work: the effect of trace elements

As we have discussed it is desirable to break this into two sections Localized corrosion and Stress corrosion cracking. If this division is used then the localized corrosion should be completed first and the results used as input for SCC tests.

Previously we have used NaCl solutions MgCl₂ solutions and LiCl solutions for testing of Alloy 22. The Catholic University tests were performed in HCl solutions where lead was added as lead acetate.

I suggest the following solutions be evaluated using the OLI software. What is needed is a determination of the free chloride concentration, the concentration of dissolved lead as well as an assessment of the type and concentration of lead complexes. Also if you feel that the suggested solution are not appropriate then please provide your input. Statistical design should be considered if we do not have to wait 2 months for an answer.

NaCl Solutions - Tested to compare the results obtained in such solutions without lead.

Cl concentrations: 0.5, 1.0, 4.0 molar

Temperatures: 80 and 100 C

J. Yang
7/10/02

lead concentration: 1, 100, 1600 (or maximum) ppm as lead chloride, lead acetate or possibly another soluble lead salt but not lead nitrate

The strategy would be to look at the most aggressive conditions first. If there is no effect in the Cl solutions at 100 C with 1600 ppm lead then there is probably not a need to look at lower lead concentrations.

Number of tests 3 for initial screening, 18 for total matrix.

LiCl solution - used to look at high Cl concentrations

Cl concentrations: 6 and 9 molal

Temperatures: 80, 100 and 120 C (6 molal LiCl boiling point?)

lead concentration: 1, 100, 1600 (or maximum) ppm

HCl solutions - used for direct comparison to Catholic University tests

Cl concentrations: 1 and 5 molar

Temperatures: 80 and 100 and

lead concentration: 1, 100, 1600 (or maximum) ppm.

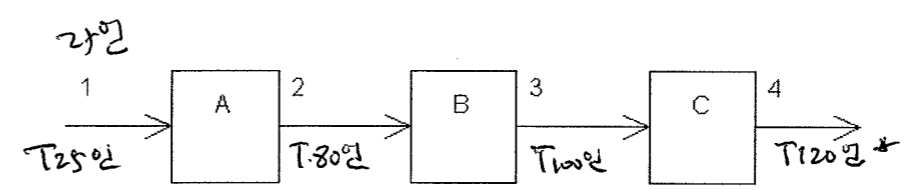
For the initial calculations it is desirable to know how much lead we can have dissolved as Pb²⁺ in the chloride solutions considering the limited solubility of lead chloride and the possible formation of lead chloride complexes.

Lead Chloride

Streams | Output Device | Exit

Using OLI 6.2e.

3 conventional mixers. to get 3 temperature at one shot.



T_{25°C}, T_{80°C}, T_{100°C}, T_{120°C} are the stream names.

We do thermo calculation.

Process Name: Darvell

Chemistry Name: Darvell1

- H₂O
- NaCl
- PbCl₂
- PbAcet₂
- PbSO₄
- LiCl
- HCl

J. Yano
8/14/02

Results: File Name: Darrell-Pb-Chem.xls directory.

in c:\work\cslt

Results from ESP V6.2e, April 10, 2001
Pb MW= 207.2 mg (ppm)
mM 0.0048263 0.482625 7.722008

1

2

Table with 4 columns: Case 1, 0.5 M NaCl; Case 2, 1 M NaCl; Case 3, 4 M NaCl; Case 4, 9M NaCl. Rows include H2O, NaCl, LiCl, HCl, PbCl2, Pb(CH3CO2)2, PbSO4, Total Pb, Stream Phase, Temperature, Pressure, pH, Total mol/hr, Flow Units, H2O, ACETACID, ACET2, H2SO4, HCL, SO3, LIOH, NAACET, PBACET2, PBCL2, PBO, LIACET, OHION, CLION, HION, HPBO2ION, HSO4ION, LION, LISO4ION, NAION, NASO4ION, ACETATEION, PBACET3ION, PBACETION, PBCL3ION, PBCL4ION, PBCLION, PBION, PBOHION, SO4ION, PBO4, NAACL, LIOH, LI2SO4, LI2SO4, LIACET, LIACET, LIOH, NA2SO4, NA2SO4, NA3HSO4, NAACET, NAHSO4, NAOH, PBOH2, PBOH2, Total g/hr, Volume, m3/hr, Enthalpy, cal/hr, Density, g/m3, Vapor fraction, Solid fraction, Organic fraction, Osmotic Pres, atm, Redox Pot, volts, E-Con, f/ohm-cm, E-Con, cm2/ohm-mol, Abs Visc, cP, Rel Visc, Ionic Strength.

J. Jones 8/19/02

Table with 4 columns: Case 4, 9M NaCl; Case 5, 6 M LiCl. Rows include H2O, NaCl, LiCl, HCl, PbCl2, Pb(CH3CO2)2, PbSO4, Total Pb, Stream Phase, Temperature, Pressure, pH, Total mol/hr, Flow Units, H2O, ACETACID, ACET2, H2SO4, HCL, SO3, LIOH, NAACET, PBACET2, PBCL2, PBO, LIACET, OHION, CLION, HION, HPBO2ION, HSO4ION, LION, LISO4ION, NAION, NASO4ION, ACETATEION, PBACET3ION, PBACETION, PBCL3ION, PBCL4ION, PBCLION, PBION, PBOHION, SO4ION, PBO4, NAACL, LIOH, LI2SO4, LI2SO4, LIACET, LIACET, LIOH, NA2SO4, NA2SO4, NA3HSO4, NAACET, NAHSO4, NAOH, PBOH2, PBOH2, Total g/hr, Volume, m3/hr, Enthalpy, cal/hr, Density, g/m3, Vapor fraction, Solid fraction, Organic fraction, Osmotic Pres, atm, Redox Pot, volts, E-Con, f/ohm-cm, E-Con, cm2/ohm-mol, Abs Visc, cP, Rel Visc, Ionic Strength.

J. Jones 8/19/02

3

4

	Case 6, 9 M LiCl, No solid above 25°C				Case 7, 4 M NaCl, Pb Acetate only				Case 8, 4 M NaCl, Pb Acetate only			
	T25oC	T80oC	T100oC	T120oC	T25oC	T80oC	T100oC	T120oC	T25oC	T80oC	T100oC	T120oC
Phase	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous
H2O (mol)	55.5	Boiling at			55.5				55.5			
NaCl (mol)	0	118.8	oC		4				4			
LiCl (mol)	9				0				0			
HCl (mol)	0				0				0			
PbCl2 (mol)	4.00E-03				0.00E+00				0.00E+00			
Pb(CH3CO2)2 (mol)	0.004				0.00004826				0.0004826			
PbSO4 (mol)	0.001				0				0			
Total Pb (ppm)	1551.76288				0.861102959				86.100657			
Stream	T25oC	T80oC	T100oC	T120oC	T25oC	T80oC	T100oC	T120oC	T25oC	T80oC	T100oC	T120oC
Phase	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous
Temperature, C	25	80	100	120	25	80	100	120	25	80	100	120
Pressure, atm	1	1	1	2	1	1	1	2	1	1	1	2
pH	6.84331	6.22504	6.04877	5.89815	6.96995	6.24848	6.06334	5.90814	7.57726	6.83093	6.63678	6.47545
Total mol/hr	63.7995	63.7999	63.7999	63.7999	59.774	59.774	59.774	59.774	59.7727	59.7726	59.7726	59.7726
Flow Units	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr
H2O	48.1868	48.1868	48.1868	48.1868	52.2434	52.2434	52.2434	52.2434	52.243	52.243	52.243	52.243
ACETACID	4.55E-07	3.35E-06	5.80E-06	9.35E-06	1.09E-08	6.36E-08	9.95E-08	1.47E-07	2.69E-07	1.87E-06	2.68E-06	4.04E-06
ACET2	3.81E-20	9.70E-18	4.19E-17	1.50E-16	4.27E-24	6.67E-22	2.41E-21	7.29E-21	2.61E-21	4.61E-19	1.75E-18	5.47E-18
H2SO4	1.03E-28	5.94E-27	2.17E-26	7.15E-26	8.92E-14	1.04E-11	3.94E-11	1.22E-10	2.20E-14	2.71E-12	1.05E-11	3.30E-11
HCL	4.24E-13	2.97E-11	1.00E-10	2.80E-10								
SO3	2.44E-29	1.39E-28	5.38E-06	8.89E-06								
LI0H	3.96E-07	3.07E-06										
NAACET					4.25E-06	4.63E-06	4.97E-06	5.34E-06	4.25E-04	4.65E-04	5.01E-04	5.40E-04
PBACET2	5.74E-17	1.14E-15	2.34E-15	4.17E-15	9.67E-19	3.49E-18	4.68E-18	5.75E-18	9.71E-13	3.54E-12	4.76E-12	5.90E-12
PBCL2	2.11E-08	5.29E-08	5.84E-08	5.90E-08	2.74E-08	5.64E-08	6.11E-08	6.23E-08	2.74E-06	5.64E-06	6.11E-06	6.23E-06
PBO	1.49E-17	6.47E-16	1.30E-15	2.10E-15	1.96E-14	2.44E-13	3.74E-13	4.84E-13	3.23E-11	3.57E-10	5.25E-10	6.61E-10
LIACET	0.00603542	0.005651	0.00564555	0.005684								
OHION	7.57E-08	4.59E-07	6.87E-07	9.50E-07	6.86E-08	4.50E-07	7.43E-07	1.14E-06	2.78E-07	1.72E-06	2.78E-06	4.22E-06
CLION	7.78978	7.78979	7.7898	7.7898	3.76527	3.76527	3.76527	3.76527	3.76346	3.76348	3.76348	3.76349
HION	1.74E-08	1.39E-07	2.63E-07	4.65E-07	5.77E-08	3.87E-07	6.43E-07	9.97E-07	1.43E-08	1.01E-07	1.72E-07	2.70E-07
HPBO2ION	1.42E-20	1.73E-18	4.23E-18	7.91E-18	4.67E-18	1.22E-16	2.18E-16	3.14E-16	3.11E-14	6.86E-13	1.15E-12	1.58E-12
HSO4ION	1.42E-10	2.85E-09	7.35E-09	1.76E-08								
LIION	7.80733	7.80767	7.80765	7.80759								
LISO4ION	7.08E-04	7.52E-04	7.73E-04	7.93E-04								
NAION					3.76529	3.76529	3.76529	3.76529	3.76483	3.7648	3.76476	3.76472
NASO4ION												
ACETATEION	9.10E-04	0.001292	0.0012945	0.001252	4.82E-06	4.39E-06	4.02E-06	3.60E-06	4.83E-04	4.42E-04	4.05E-04	3.64E-04
PBACET3ION	6.88E-17	1.60E-15	3.91E-15	8.61E-15	1.40E-21	3.62E-21	5.13E-21	7.03E-21	1.40E-13	3.68E-13	5.27E-13	7.30E-13
PBACETION	2.30E-13	1.12E-12	1.42E-12	1.61E-12	1.19E-13	1.69E-13	1.55E-13	1.33E-13	1.19E-09	1.70E-09	1.57E-09	1.34E-09
PBCL3ION	1.50E-05	2.93E-05	2.95E-05	2.93E-05	1.16E-07	2.31E-07	2.61E-07	2.84E-07	1.16E-05	2.31E-05	2.62E-05	2.84E-05
PBCL4ION	0.00779905	0.007785	0.00778457	0.007785	4.39E-06	4.24E-06	4.21E-06	4.19E-06	4.39E-04	4.24E-04	4.21E-04	4.19E-04
PBCLION	7.55E-10	2.16E-09	2.39E-09	2.38E-09	6.23E-09	1.06E-08	1.03E-08	9.26E-09	6.24E-07	1.06E-06	1.03E-06	9.27E-07
PBION	1.13E-13	3.08E-13	3.04E-13	2.63E-13	8.52E-11	1.05E-10	8.36E-11	6.07E-11	8.54E-09	1.05E-08	8.36E-09	6.08E-09
PBOHION	4.13E-14	1.07E-12	2.04E-12	3.21E-10	1.42E-11	1.26E-10	1.84E-10	2.32E-10	5.76E-09	4.83E-08	6.91E-08	8.58E-08
SO4ION	1.60E-04	1.16E-04	9.49E-05	7.57E-05								
PBSO4												
NACL												
LI2SO4.1H2O												
LI2SO4												
LIACET.2H2O												
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LI2SO4												

Page 1 through 68

are submitted for printing (photo copying)

on April 04/11/01 04/11/01

J. Yang

04/11/01

April 19/01

conductivity calculation to know if

conductivity method would allow the measurement of deliquescence point for mixtures of salt.

J. Yang
2/10/02

File Name: NaNO3_NaCl_Conductivity_Weight.xls, Directory: Notebook#430
OLI 6.2d simulation, April 18, 2001
Dependence of electrical conductivity, weight loss on relative humidity at 25oC
Chemistry Model
H2O +NaCl +NaNO3

	Case 1			Case 2			Case 3			Case 4			Case 5		
	In	out		In	out		In	out		In	out		In	out	
RH *			0.6937 RH			0.6989			0.7039			0.7181			0.7391
E-Con, 1/ohm-cm			0.2272 Conductivity			0.2271			0.2269			0.2263			0.2246
H2O total (Mol/h)			55.408008			56.408008			57.408008			60.408008			65.408008
H2O total (g/h)			997.34414			1015.3441			1033.3441			1087.3441			1177.3441
Total g/hr			1751.4847			1769.5028			1787.5208			1841.5648			1931.6349
Fraction (NaCl/NaNO3)			0.3061224			0.3061224			0.3061224			0.3061224			0.3061224
* Note: 0.6937 is from Notebook #430 page 55															
Stream	In	out	out	In	out	out	In	out	out	In	out	out	In	out	out
Phase	Aqueous	Aqueous	Vapor	Aqueous	Aqueous	Vapor	Aqueous	Aqueous	Vapor	Aqueous	Aqueous	Vapor	Aqueous	Aqueous	Aqueous
Temperature, C	25	25	25	25	25	25	25	25	25	25	25	25	25	25	25
Pressure, atm	1	0.0217784	0.021778	1	0.0219417	0.021942	1	0.0220999	0.0221	1	0.0225457	0.022546	1	0.0232045	1
pH	7.00101	7.00123	7.00116	7.00116	7.00138	7.00138	7.0013	7.00152	7.00167	7.00167	7.00188	7.00215	7.00215	7.00237	7.00237
Total mol/hr	65.208	65.1428	0.065208	66.208	66.1418	0.066208	67.208	67.1408	0.067208	70.208	70.1378	0.070208	75.208	75.1328	75.1328
Flow Units	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr
H2O	55.408	55.3428	0.065208	56.408	56.3418	0.066208	57.408	57.3408	0.067208	60.408	60.3378	0.070208	65.408	65.3328	65.3328
H2			5.88E-28			5.95E-28			6.03E-28			6.26E-28			6.26E-28
HCL	8.70E-14	8.69E-14	8.25E-13	8.72E-14	8.71E-14	8.02E-13	8.73E-14	8.73E-14	7.81E-13	8.77E-14	8.77E-14	7.26E-13	8.83E-14	8.82E-14	8.82E-14
HNO3	1.13E-09	1.13E-09	1.87E-12	1.18E-09	1.18E-09	1.86E-12	1.24E-09	1.23E-09	1.84E-12	1.40E-09	1.39E-09	1.80E-12	1.68E-09	1.67E-09	1.67E-09
O2			2.94E-28			2.98E-28			3.01E-28			3.13E-28			3.13E-28
NaNO3	6.8	6.8	6.8	6.8	6.8	6.8	6.8	6.8	6.8	6.8	6.8	6.8	6.8	6.8	6.8
NaCl	3	3	3	3	3	3	3	3	3	3	3	3	3	3	3
NaOH.1H2O															
NaOH	1.13E-09	1.13E-09	1.18E-09	1.18E-09	1.18E-09	1.24E-09	1.24E-09	1.24E-09	1.24E-09	1.40E-09	1.40E-09	1.40E-09	1.68E-09	1.68E-09	1.68E-09
Total g/hr	1751.49	1750.31	1.17474	1769.5	1768.31	1.19276	1787.52	1786.31	1.21077	1841.56	1840.3	1.26482	1931.64	1930.28	1930.28
Volume, m3/hr	0.001292	0.0012907	0.073232	0.00131	0.0013084	0.073801	0.001327	0.0013261	0.07438	0.001381	0.0013793	0.076163	0.001469	0.0014681	0.0014681
Enthalpy, cal/hr	-4.80E+06	-4.80E+06	-3768.91	-4.87E+06	-4.87E+06	-3826.71	-4.94E+06	-4.93E+06	-3884.51	-5.14E+06	-5.14E+06	-4057.9	-5.49E+06	-5.48E+06	-5.48E+06
Density, g/m3	1.36E+06	1.36E+06	16.0414	1.35E+06	1.35E+06	16.1618	1.35E+06	1.35E+06	16.2783	1.33E+06	1.33E+06	16.6068	1.31E+06	1.31E+06	1.31E+06
Vapor fraction															
Solid fraction															
Organic fraction															
Osmotic Pres, atm	517.429	518.126	506.664	506.664	507.343	496.316	496.316	496.979	467.556	467.556	468.175	426.116	426.671	426.671	
Redox Pot, volts	0.403347	0.407497	0.403274	0.403274	0.407424	0.403205	0.403205	0.407355	0.403012	0.407162	0.402737	0.406887	0.406887		
E-Con, 1/ohm-cm	0.227158	0.227163	0.22705	0.22705	0.227058	0.226902	0.226902	0.226913	0.226249	0.226267	0.224582	0.22461	0.22461		
E-Con, cm2/ohm-mol	29.9436	29.9187	30.3398	30.3398	30.3149	30.7307	30.7307	30.7057	31.8715	31.8464	33.6799	33.6488	33.6488		
Abs Visc, cP	2.46794	2.47063	2.42583	2.42583	2.42844	2.38565	2.38818	2.38818	2.27266	2.27508	2.11083	2.11293	2.11293		
Rel Visc	2.77073	2.77375	2.72346	2.72346	2.72638	2.67835	2.68118	2.68118	2.55148	2.5542	2.3698	2.37216	2.37216		
Ionic Strength	9.72259	9.73405	9.55022	9.55022	9.56144	9.38388	9.38388	9.39487	8.918	8.918	8.92837	8.23676	8.24623		

J. Yang
04/11/01

J. Yang
8/10/02

J.Y. 04/19/01

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0.6883
0.2272
54.408008
979.34414
1733.4667
0.3061224

0.6828
0.2272
53.408008
961.34414
1715.4587
0.3061224

0.6770
0.2272
52.408008
943.34414
1697.4407
0.3061224

0.6759
0.2272
52.208008
939.74414
1693.8371
0.3061224

0.6750
0.2272
52.057958
937.04324
1691.1344
0.3061224

Case 6			Case 7			Case 8			Case 9			Case 10		
In	out		In	out		In	out		In	out		In	out	
Aqueous	Aqueous	Vapor	Aqueous	Aqueous	Vapor	Aqueous	Aqueous	Vapor	Aqueous	Aqueous	Vapor	Aqueous	Aqueous	Vapor
25	25	25	25	25	25	25	25	25	25	25	25	25	25	25
0.029205	7.00086	0.0216096	0.02161	7.0007	0.0214352	0.021435	7.00052	0.021255	7.00049	0.0212181	0.021218	7.00046	7.00069	0.02119
0.075208	64.208	64.1438	0.064208	63.208	63.1448	0.063208	62.208	62.1458	62.008	61.946	0.062208	61.858	61.7961	0.061858
mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr
54.408	54.3438	53.4448	53.408	53.3448	5.73E-28	5.73E-28	52.408	52.3458	52.208	52.146	0.062208	52.058	51.9961	0.061858
6.64E-28	5.80E-28	5.80E-28	5.80E-28	5.73E-28	5.73E-28	5.73E-28	5.65E-28	5.65E-28	5.65E-28	5.64E-28	5.64E-28	5.64E-28	5.63E-28	5.63E-28
6.51E-13	8.68E-14	8.48E-13	8.66E-14	8.66E-14	8.74E-13	8.64E-14	8.64E-14	8.64E-14	8.64E-14	9.06E-13	8.64E-14	8.64E-14	8.63E-14	9.10E-13
1.75E-12	1.08E-09	1.07E-09	1.03E-09	1.02E-09	1.90E-12	9.77E-10	9.73E-10	9.73E-10	9.68E-10	1.93E-12	9.63E-10	9.59E-10	9.59E-10	1.93E-12
3.32E-28	6.8	6.8	6.8	6.8	2.86E-28	2.86E-28	6.8	6.8	6.8	2.83E-28	2.83E-28	6.8	6.8	2.81E-28
	3	3	3	3			3	3	3			3	3	3
1.08E-09	1.08E-09	1.03E-09	1.03E-09	1.03E-09	9.77E-10	9.76E-10	9.77E-10	9.76E-10	9.67E-10	9.66E-10	9.66E-10	9.59E-10	9.58E-10	1.11439
1.35489	1733.47	1732.31	1.15673	1715.46	1714.32	1.13871	1697.44	1696.32	1.1207	1693.84	1692.72	1.11709	1691.13	1690.02
0.07927	0.001274	0.001273	0.072672	0.001256	0.0012553	0.072123	0.001239	0.0012377	0.071584	0.001235	0.0012341	0.071478	0.0012315	0.071398
-4346.89	-4.73E+06	-4.73E+06	-3711.11	-4.67E+06	-4.66E+06	-3653.31	-4.60E+06	-4.59E+06	-3595.51	-4.58E+06	-4.58E+06	-3583.95	-4.57E+06	-3575.28
17.0922	1.36E+06	1.36E+06	15.9171	1.37E+06	1.37E+06	15.7886	1.37E+06	1.37E+06	15.6557	1.37E+06	1.37E+06	15.6286	1.37E+06	15.6081
	6.8	6.8	6.8	6.8	6.8	6.8	6.8	6.8	6.8	6.8	6.8	6.8	6.8	6.8
	3	3	3	3	3	3	3	3	3	3	3	3	3	3
528.637	529.352	541.048	540.315	541.048	552.49	553.243	552.49	553.243	554.988	555.744	555.744	556.875	557.634	557.634
0.403422	0.407572	0.407651	0.403501	0.407651	0.403584	0.407734	0.403584	0.407734	0.4036	0.407751	0.407751	0.403613	0.407763	0.407763
0.227225	0.227227	0.227246	0.227247	0.227246	0.227221	0.227218	0.227221	0.227218	0.22721	0.227206	0.227206	0.2272	0.227196	0.227196
29.5417	29.5169	29.1094	29.1342	29.1094	28.7208	28.6961	28.7208	28.6961	28.6374	28.6127	28.6127	28.5747	28.55	28.55
2.51211	2.51489	2.56138	2.5585	2.56138	2.60729	2.61026	2.60729	2.61026	2.61735	2.62035	2.62035	2.62496	2.62798	2.62798
2.82032	2.82344	2.87563	2.8724	2.87563	2.92717	2.93051	2.92717	2.93051	2.93847	2.94183	2.94183	2.94701	2.9504	2.9504
9.90132	9.91302	10.0868	10.0868	10.0987	10.2793	10.2916	10.2793	10.2916	10.3187	10.331	10.331	10.3485	10.3608	10.3608

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0.6741
0.2272
51.908008
934.34414
1688.4317
0.3061224

0.6735
0.2272
51.708008
930.74414
1684.8259
0.3061362

0.6728
0.2272
51.608008
928.94414
1683.0328
0.3067249

J.Y. 04/19/01

Case 11			Case 12			Case 13			Case 14		
In	out		In	out		In	out		In	out	
Aqueous	Aqueous	Vapor	Aqueous	Aqueous	Vapor	Aqueous	Aqueous	Vapor	Aqueous	Aqueous	Vapor
25	25	25	25	25	25	25	25	25	25	25	25
1.0211624	7.00066	0.021162	0.021162	7.00042	0.021144	0.0211254	0.021125	0.021125	7.00033	0.0211222	0.021122
0.075208	61.6483	0.061708	61.608	61.5464	0.061608	61.508	61.4461	4.37E-04	0.061508	61.4003	0.007688
mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr
51.908	51.8463	0.061708	51.808	51.7464	0.061608	51.708	51.6465	51.608	51.5466	51.5466	0.061408
6.62E-28	5.62E-28	5.62E-28	5.61E-28	5.61E-28	5.61E-28	5.60E-28	5.60E-28	5.60E-28	5.60E-28	8.62E-14	5.59E-28
8.63E-14	8.63E-14	9.15E-13	8.63E-14	8.63E-14	8.63E-14	8.63E-14	8.62E-14	8.62E-14	9.20E-13	8.63E-14	9.21E-13
9.51E-10	9.48E-10	1.93E-12	9.46E-10	9.43E-10	1.93E-12	9.41E-10	9.38E-10	1.93E-12	9.37E-10	9.35E-10	1.93E-12
2.81E-28	2.81E-28	2.80E-28	2.80E-28	2.80E-28	2.80E-28	2.80E-28	2.80E-28	2.80E-28	2.80E-28	2.80E-28	2.80E-28
6.8	6.8	6.8	6.8	6.8	6.8	6.8	6.8	6.8	6.8	6.8	6.8
3	3	3	3	3	3	3	3	3	3	3	3
9.52E-10	9.51E-10	9.46E-10	9.47E-10	9.46E-10	9.42E-10	9.41E-10	9.41E-10	9.41E-10	9.34E-10	1682.37	1.63648
1688.43	1687.32	1.11169	1686.63	1685.52	1.10989	1684.83	1683.68	0.037137	1.10809	1682.37	1.63648
0.00123	0.0012288	0.071319	0.001228	0.0012271	0.071266	0.001226	0.0012253	1.65E-08	0.071213	2.90E-07	7.25E-07
-4.56E+06	-4.56E+06	-3566.61	-4.56E+06	-4.55E+06	-3560.83	-4.55E+06	-4.54E+06	-48.8416	-3555.05	-4.54E+06	-859.34
1.37E+06	1.37E+06	15.5876	1.37E+06	1.37E+06	15.5738	1.37E+06	1.37E+06	2.26E+06	15.5602	1.37E+06	2.26E+06
558.774	559.537	560.047	560.047	560.812	561.326	562.068	562.185	562.185	562.185	562.185	562.185
0.403626	0.407776	0.403635	0.403635	0.407785	0.403643	0.407794	0.403652	0.403652	0.403652	0.403652	0.403652
0.227189	0.227185	0.227181	0.227181	0.227176	0.227173	0.227169	0.227169	0.227169	0.227194	0.227194	0.227234
28.5119	28.4872	28.4699	28.4699	28.4452	28.4279	28.4031	28.3833	28.3833	28.3548	28.3548	28.3548
2.63264	2.63567	2.63779	2.63779	2.64083	2.64296	2.6459	2.6459	2.6459	2.64614	2.64614	2.64615
2.95563	2.95903	2.96141	2.96141	2.96483	2.96722	2.97052	2.97052	2.97052	2.97079	2.97079	2.9708
10.3784	10.3908	10.3984	10.3984	10.4108	10.4186	10.4305	10.4305	10.4305	10.4306	10.4306	10.4308

P.g. 04/19/01

0.6721
0.2277
50.90801
916.3441
1670.418
0.310909

0.6726
0.2274
51.408008
925.34414
1679.427
0.3079096

Case 15				Case 16				Case 17			
In	In	out	out	In	In	out	out	In	In	out	out
Aqueous	Solid	Aqueous	Solid	Aqueous	Solid	Vapor	Solid	Aqueous	Solid	Aqueous	Solid
25	25	25	25	25	25	25	25	25	25	25	25
7.0007	1	0.0211157	0.021116	6.99954	1	0.021099	0.021099	6.99872	1	0.0210827	0.021083
61.1627	0.045353	61.0899	0.056878	60.5685	0.139459	0.061208	0.061208	59.9745	0.233479	59.903	0.244795
51.408	mol/hr	51.3468	mol/hr	50.908	mol/hr	50.8473	mol/hr	50.408	mol/hr	50.3478	mol/hr
8.62E-14		5.58E-28		8.59E-14		5.59E-28		8.57E-14		5.49E-28	
9.31E-10		9.24E-13		9.13E-10		1.90E-12		8.98E-10		1.88E-12	
		1.93E-12		9.13E-10		2.77E-28		8.98E-10		2.74E-28	
6.75465	0.045353	6.74312	0.056878	6.66054	0.139459	6.64912	0.150879	6.56652	0.233479	6.55521	0.244795
3		3		3		3		3		3	
8.66E-10		9.17E-10		9.17E-10		9.17E-10		9.01E-10		9.01E-10	
1675.57	3.85479	1673.49	4.83432	1658.56	11.8533	1656.5	12.824	1641.57	19.8445	1639.52	20.8063
0.001219	1.71E-06	0.001218	2.14E-06	0.001207	5.25E-06	0.001206	5.68E-06	0.001195	8.79E-06	0.0011937	9.22E-06
-4.52E+06	-5069.72	-4.52E+06	-6357.97	-15589.1	-4.47E+06	-16865.7	-3508.82	-4.44E+06	-26099	-4.43E+06	-27363.9
1.37E+06	2.26E+06	1.37E+06	2.26E+06	2.26E+06	2.26E+06	1.37E+06	2.26E+06	1.37E+06	2.26E+06	1.37E+06	2.26E+06
562.678		563.932		564.064		564.064		565.216		565.35	
0.40367		0.403717		0.407867		0.407867		0.403764		0.407914	
0.227323		0.227652		0.227652		0.227652		0.227986		0.228027	
28.2866		28.0448		28.0166		28.0166		27.8031		27.7752	
2.64663		2.6479		2.64791		2.64791		2.64922		2.64923	
2.97134		2.97277		2.97278		2.97278		2.97425		2.97426	
10.4311		10.4323		10.4325		10.4325		10.4337		10.4338	

P.g. 04/19/01

0.6668
0.2310
46.408008
835.34414
1589.3465
0.3406261

0.6693
0.2294
48.408008
871.34414
1625.3768
0.3267814

Case 18				Case 19				Case 20			
In	In	out	out	In	In	out	out	In	In	out	out
Aqueous	Solid	Aqueous	Solid	Aqueous	Solid	Vapor	Solid	Aqueous	Solid	Aqueous	Solid
25	25	25	25	25	25	25	25	25	25	25	25
6.99586	1	0.0210117	0.021012	6.99276	1	0.0209333	0.020933	6.99111	1	0.0208909	0.020891
57.5994	0.60865	57.5303	0.619546	55.2258	0.98222	0.058208	0.058208	54.0397	1.16834	53.9742	1.1786
48.408	mol/hr	48.3498	mol/hr	46.408	mol/hr	46.3518	mol/hr	45.408	mol/hr	45.3528	mol/hr
8.50E-14		5.31E-28		8.40E-14		5.13E-28		8.35E-14		5.05E-28	
8.39E-10		9.46E-13		8.41E-14		9.65E-13		7.46E-10		9.74E-13	
		1.81E-12		7.78E-10		1.73E-12		7.46E-10		1.69E-12	
		2.66E-28		2.66E-28		2.57E-28		2.57E-28		2.52E-28	
6.19135	0.60865	6.18045	0.619546	5.81778	0.98222	5.80731	0.992693	5.63166	1.16834	5.6214	1.1786
3		3		3		3		3		3	
8.39E-10		8.40E-10		7.78E-10		7.79E-10		7.48E-10		7.49E-10	
1573.65	51.7321	1571.67	52.6582	1505.86	83.4837	1503.96	84.3739	1472.03	99.3026	1470.16	100.175
0.001147	2.29E-05	0.0011451	2.33E-05	0.001098	3.70E-05	0.0010966	3.74E-05	0.001074	4.40E-05	0.0010724	4.44E-05
-4.26E+06	-68036.7	-4.25E+06	-69254.7	-3364.32	-4.08E+06	-1.10E+05	-3248.72	-3.99E+06	-1.31E+05	-3.99E+06	-1.32E+05
1.37E+06	2.26E+06	1.37E+06	2.26E+06	1.37E+06	2.26E+06	1.37E+06	2.26E+06	1.37E+06	2.26E+06	1.37E+06	2.26E+06
570.683		576.741		576.896		576.896		580.022		580.184	
0.403962		0.404177		0.408328		0.408328		0.404292		0.408443	
0.229393		0.229436		0.230965		0.230965		0.231734		0.23178	
26.8369		26.8099		25.8454		25.8454		25.3892		25.3636	
2.65501		2.65504		2.6618		2.6618		2.66554		2.6656	
2.98074		2.98078		2.98831		2.98837		2.99257		2.99264	
10.4404		10.4406		10.4496		10.4499		10.4554		10.4557	

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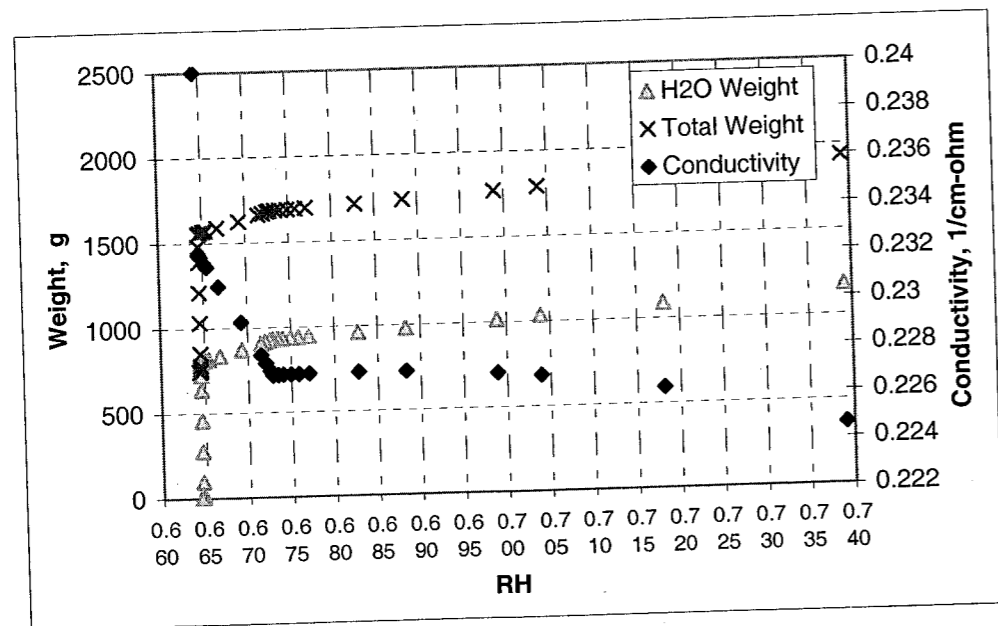
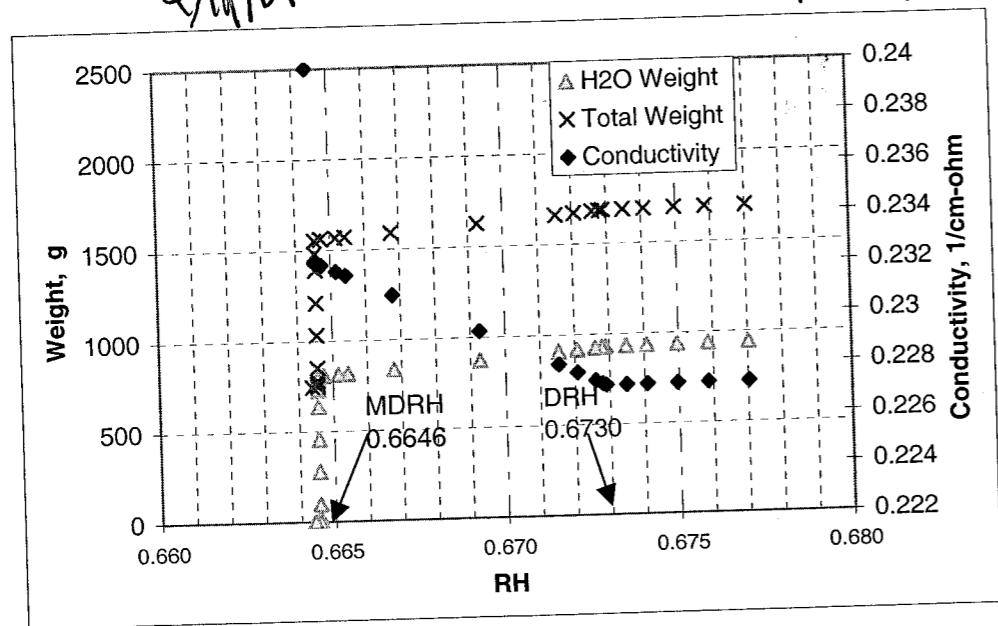
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0.2323
44.408008
808.34414
1562.3256
0.3517564

0.6646
0.2322
44.408008
808.34414
1562.3256
0.3517564

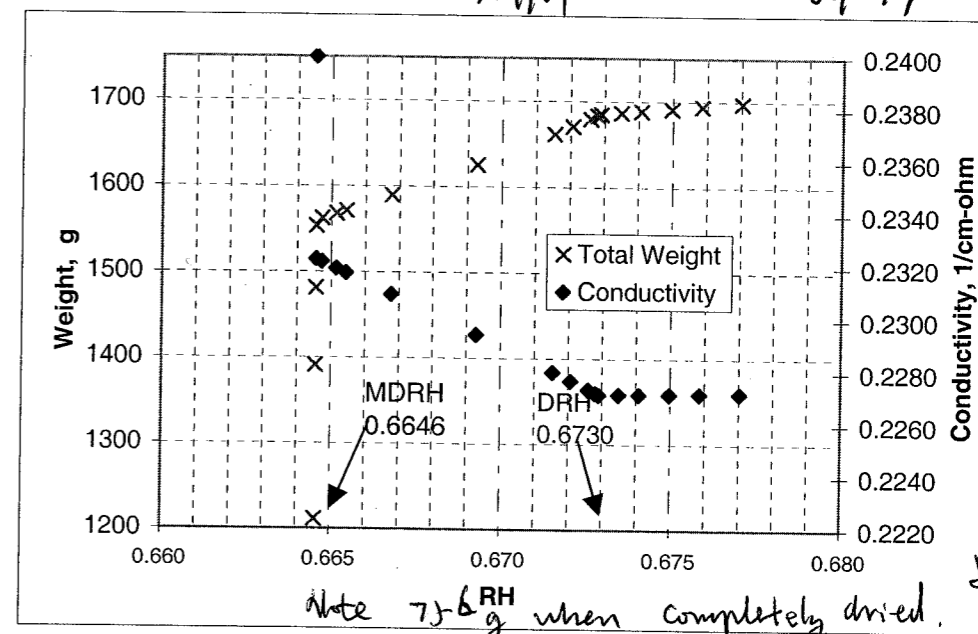
0.6646
0.2323
44.408008
799.34414
1553.3196
0.352691

Case 21				Case 22				Case 23			
In	In	out	out	In	In	out	out	In	In	out	out
Aqueous	Solid	Aqueous	Solid	Aqueous	Solid	Vapor	Solid	Aqueous	Solid	Aqueous	Solid
25	25	25	25	25	25	25	25	25	25	25	25
6.99078	1.2055	53.7373	1.21572	6.99027	53.3819	1.27137	0.054708	6.98996	52.8525	1.35547	52.788
mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr	mol/hr
45.208	45.153	5.03E-28	0.055008	44.908	44.8533	0.054708	44.408	44.3538	44.408	44.3538	0.054208
8.35E-14	8.34E-14	9.76E-13	8.33E-14	8.33E-14	8.33E-14	5.00E-28	9.80E-13	8.25E-14	8.27E-14	8.25E-14	4.96E-28
7.42E-10	7.40E-10	1.68E-12	7.33E-10	7.31E-10	7.31E-10	1.67E-12	7.22E-10	7.21E-10	7.22E-10	7.21E-10	9.74E-13
5.5945	1.2055	5.58428	1.21572	5.59879	1.26121	2.50E-28	5.46601	5.45954	5.46601	5.45954	2.48E-28
3	3	3	3	3	3	1.27137	2.97852	2.97467	2.97852	2.97467	0.025533
7.42E-10	7.43E-10	1465.27	102.462	7.33E-10	7.34E-10	103.33	0.990986	1436.68	114.638	115.413	0.976573
1465.27	102.462	1463.41	103.33	1455.13	107.197	108.06	0.985581	1436.93	115.413	115.413	0.976573
0.001069	4.54E-05	0.0010676	4.58E-05	0.001062	4.75E-05	0.064119	0.001063	0.0010484	5.08E-05	5.12E-05	0.068549
-3.98E+06	-1.35E+05	-3.97E+06	-1.36E+05	-3.95E+06	-1.41E+05	-3.179.37	-3.95E+06	-3.90E+06	-1.51E+05	-1.52E+05	-3133.13
1.37E+06	2.26E+06	1.37E+06	2.26E+06	1.37E+06	2.26E+06	15.381	1.37E+06	1.37E+06	2.26E+06	2.26E+06	15.3672
580.7	580.863	0.404315	0.408467	0.231948	25.2927	2.66633	2.99346	10.4566	581.897	0.408502	0.232201
0.404315	0.408467	0.231948	25.2927	2.66633	2.99346	10.4566	581.897	0.408502	0.232201	25.1481	2.66755
25.2927	2.66633	2.99346	10.4566	581.897	0.408502	0.232201	25.1481	2.66755	2.99483	2.99547	10.4597
2.66633	2.99346	10.4566	581.897	0.408502	0.232201	25.1481	2.66755	2.99483	10.4585	10.4597	582.322
2.99346	10.4566	581.897	0.408502	0.232201	25.1481	2.66755	2.99483	10.4585	582.322	0.408517	0.232306
10.4566	581.897	0.408502	0.232201	25.1481	2.66755	2.99483	10.4585	581.897	0.408517	0.232306	24.8525
581.897	0.408502	0.232201	25.1481	2.66755	2.99483	10.4585	581.897	0.408502	0.232306	24.8525	2.66829
0.408517	0.232306	24.8525	2.66829	2.99547	10.4597	582.322	0.408517	0.232306	24.8525	2.66829	2.99547
24.8525	2.66829	2.99547	10.4597	582.322	0.408517	0.232306	24.8525	2.66829	2.99547	10.4597	10.4597
2.66829	2.99547	10.4597	582.322	0.408517	0.232306	24.8525	2.66829	2.99547	10.4597	582.322	0.408517
2.99547	10.4597	582.322	0.408517	0.232306	24.8525	2.66829	2.99547	10.4597	582.322	0.408517	0.232306
10.4597	582.322	0.408517	0.232306	24.8525	2.66829	2.99547	10.4597	582.322	0.408517	0.232306	14.217
582.322	0.408517	0.232306	24.8525	2.66829	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812
0.408517	0.232306	24.8525	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812	2.99547
0.232306	14.217	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812	2.99547	10.4597
22.6134	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322
2.66812	2.99547	10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322	0.408517
2.99547	10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322	0.408517	0.232306
10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217
582.322	0.408517	0.232306	14.217	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812
0.408517	0.232306	14.217	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812	2.99547
0.232306	14.217	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812	2.99547	10.4597
22.6134	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322
2.66812	2.99547	10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322	0.408517
2.99547	10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322	0.408517	0.232306
10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217
582.322	0.408517	0.232306	14.217	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812
0.408517	0.232306	14.217	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812	2.99547
0.232306	14.217	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812	2.99547	10.4597
22.6134	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322
2.66812	2.99547	10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322	0.408517
2.99547	10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322	0.408517	0.232306
10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217
582.322	0.408517	0.232306	14.217	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812
0.408517	0.232306	14.217	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812	2.99547
0.232306	14.217	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812	2.99547	10.4597
22.6134	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322
2.66812	2.99547	10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322	0.408517
2.99547	10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322	0.408517	0.232306
10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217
582.322	0.408517	0.232306	14.217	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812
0.408517	0.232306	14.217	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812	2.99547
0.232306	14.217	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812	2.99547	10.4597
22.6134	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322
2.66812	2.99547	10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322	0.408517
2.99547	10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322	0.408517	0.232306
10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217
582.322	0.408517	0.232306	14.217	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812
0.408517	0.232306	14.217	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812	2.99547
0.232306	14.217	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812	2.99547	10.4597
22.6134	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322
2.66812	2.99547	10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322	0.408517
2.99547	10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322	0.408517	0.232306
10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217
582.322	0.408517	0.232306	14.217	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812
0.408517	0.232306	14.217	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812	2.99547
0.232306	14.217	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	14.217	2.66812	2.99547	10.4597
22.6134	2.66812	2.99547	10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4597	582.322
2.66812	2.99547	10.4597	582.322	0.408517	0.232306	22.6134	2.66812	2.99547	10.4		

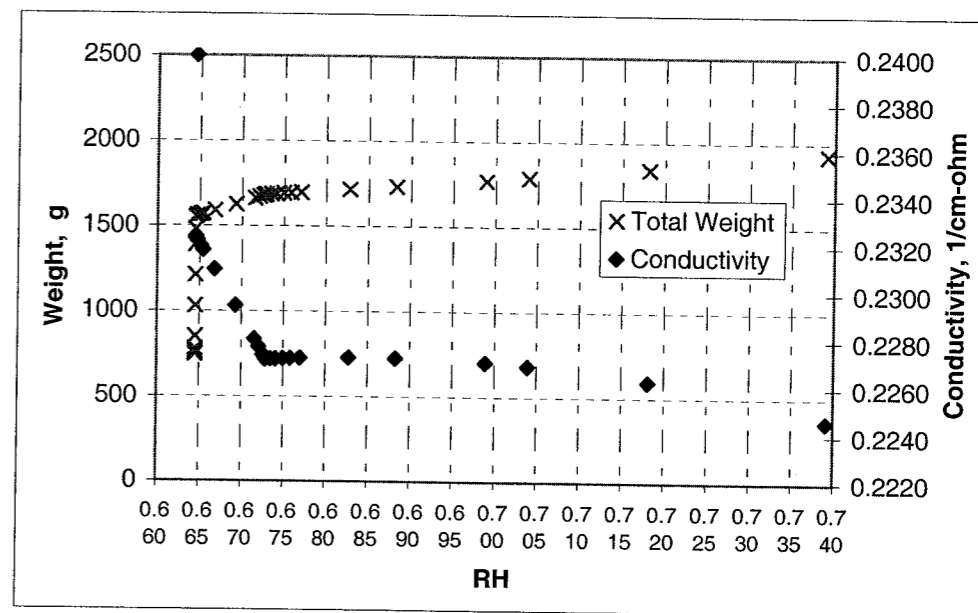
J.Y. 4/14/01 Results see pages 69-77



J.Y. 4/19/01 Results see pages 69-77



Note 75.6g when completely dried. J.Y.



Compare Results on page 55.

YM waters Evaporation

Lietai Yang

From: Lauren Browning [lbrowning@gargol.cnwra.swri.edu]
Sent: Wednesday, April 18, 2001 3:21 PM
To: Lietai Yang
Subject: waters

Lietai,

This should give you a start, anyway. You might try running these with different fixed values of CO2(g). I'd suggest fixing the log f CO2 to -3 and -3.5 to start. These are measured CO2 gas pressures in the matrix pores, and atmospheric. It would also be interesting at some point to try a closed system (i.e. don't fix the p CO2(g), but let it be consumed).

Table with columns: Species, units, Init.PoreWater, PERM-2, PERM-3, Infiltration. Rows include HCO3-, redox, Mg++, SiO2(aq), K+, Al+++ (circled), SO4--, Ca++, Fe++, Na+, Cl-, pH, T=, Reference: NO3.

Handwritten notes: mso2 = 60, 1.175, 1.1, 1.25, 1.175 mmol/L, AlCl3, MAl = 27, 3.67E-8, 3.67E-8, 3.67E-8, 9.78E-7 mmol/L

Handwritten note: given by Lauren by phone.

References: 1)CRWMS M&O, Drift-Scale Coupled Processes (DST and THC Seepage) Models, MDL-NB

Handwritten note: I added these to 1 No F. 5/18/01

S-HS-000001, Revision 01 ICN 01, Las Vegas, NV, Office of Civilian Radioactive Waste Management &

System, Management and Operating Contractor, 2000.

Handwritten signature: J. Yang

April 20/01

Data Reconcile:

1) Init. pore water

Template Reconcile Units LastResult Help

Software interface screenshot showing 'Lauren Study J13 Model Concentrations' and a table of ion concentrations (Cations and Anions) with Input and Reconciled values.

File Name: LB_pore

Calc. pH: 7.33417

added no3

to add: SiO2 and CO2 later

add AlCl3 too

Handwritten signature: J. Yang

04/23/01

② Perm-2 water

Template Reconcile Units LastResult Help

LAUREN Study
J13 Model
Concentrations

Values in mg/l

Cations	Input	Reconciled	Anions	Input	Reconciled
CA+2	106.	105.995	CL-1	110.	109.995
K+1	7.	6.99968	F-1	200.	245.642
MG+2	16.6	16.5992	HCO3-1	3.	2.99986
NA+1	61.	60.9972	NO3-1	111.	110.995
			SO4-2		

added by.

<PgDn>

Calculate pH Reconcile pH Help

LAUREN Study
J13 Model
Sample LB_PM-2

Sample LB_PM-2

Measured pH: 0.0

Calculated pH: 7.25418

Sample: LB_PM-2
J. Jones
alun/or

04/23/01

Template Reconcile Units LastResult Help

LAUREN Study
J13 Model
Concentrations

Values in mg/l

Cations	Input	Reconciled	Anions	Input	Reconciled
CA+2	97.	97.0002	CL-1	123.	123.
K+1	9.	8.99999	F-1	187.346	187.346
MG+2	17.4	17.4	HCO3-1	10.	10.
NA+1	62.	61.9999	NO3-1	120.	120.
			SO4-2		

Reduced from 200 mg/l. J.J.

<PgDn>

Calculate pH Reconcile pH Help

LAUREN Study
J13 Model
Sample LB_PM_3

Sample LB_PM_3

Measured pH: 0.0

Calculated pH: 7.37052

J. Jones
alun/or

Template Reconcile Units LastResult Help

LAUREN Study
J13 Model
Concentrations

Values in mg/l

Cations	Input	Reconciled	Anions	Input	Reconciled
CA+2	101.	101.	CL-1	118.	118.
K+1	8.	7.99999	F-1	211.228	211.229
MG+2	17.	17.	HCO3-1	6.5	6.49997
NA+1	61.3	61.3	NO3-1	116.	116.
			SO4-2		

Reduced from 216 mg/l
↓ y.

Calculate pH Reconcile pH Help

LAUREN Study
J13 Model
Sample LB_INFIL

Sample LB_INFIL

Measured pH: 0.0

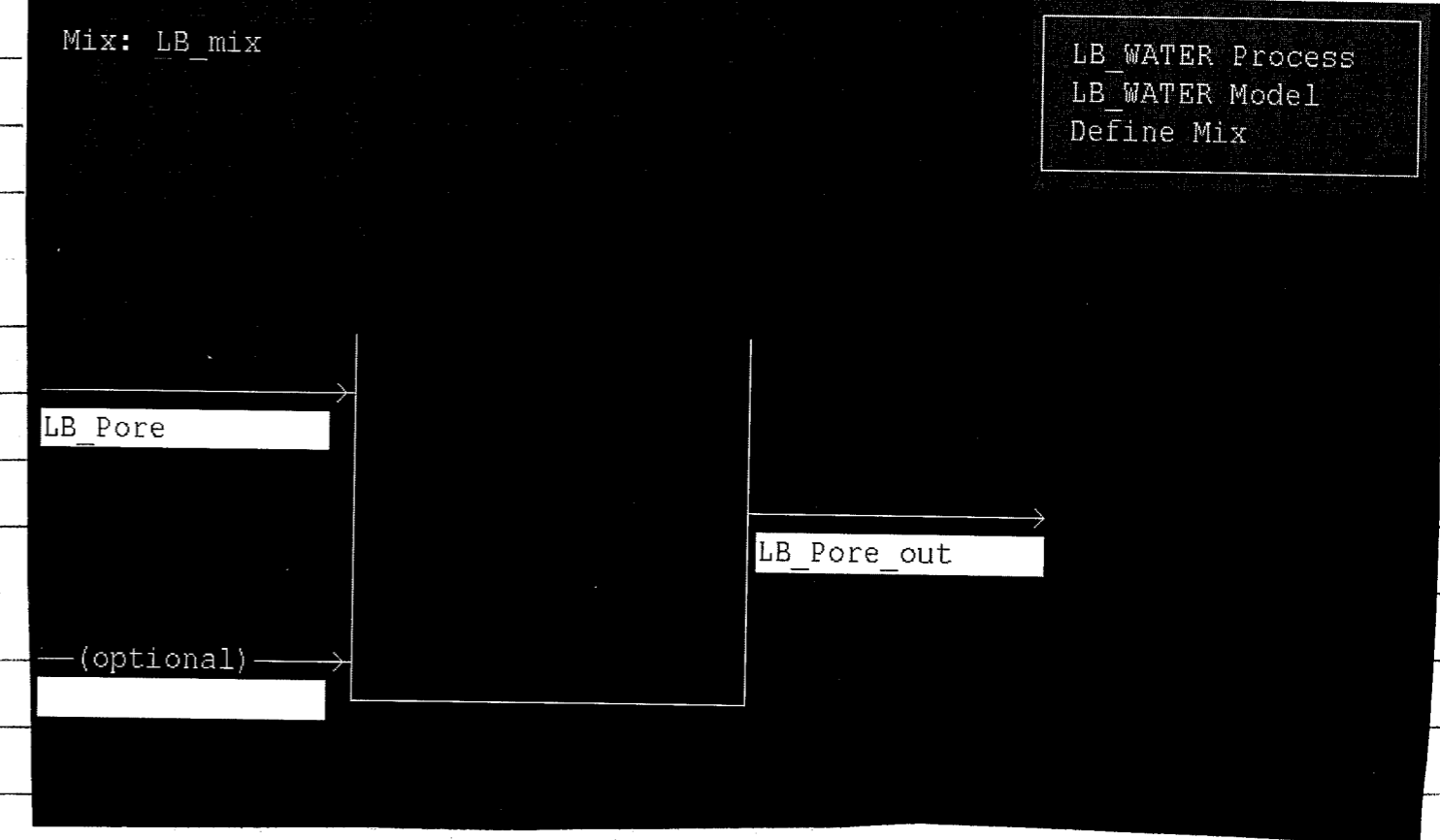
Calculated pH: 7.3172

J. J. J.
2/10/01

Simulation using OLI V6.2 e
using water reconciled on pages 81, 82, 83, 84.

Evaporate the water in a mixer to 48% ↓ y. 04/23/01
48% of vapour.

File Config Parameters Units Process Check Memo Help



Mix Equilibrium Calc

T, Vapor Fraction Equilibrium Calculation

Temperature 90. C
Vapor Fraction 0.98 molar

Either enter the pressure or pressure drop when specifying a pressure.

Blank pressure defaults to inlet conditions.

J. J. J.
2/10/01

Dummy simulation, SiO2, AlCl3 as shown in page 80, were added.

04/23/01

04/23/01

File: Lb_Waters.xls
 Perm-3: Reconciled 04/21/01, Note Book Page 83
 Additional: SiO2 75 mg, AlCl3 3.67E-8 molal, 9.92e-7 mg/L for Al

Case 1	Input CO2 = 0 (molal) = 0 (mg)	logPCO2 = -4.589272	Case 2	Input CO2 = 0.02 (molal) = 880 (mg)	logPCO2 = -3.565348	Case 3	Input CO2 = 0.065 (molal) = 2860 (mg)	logPCO2 = -3.078894
Stream Phase	LB_PM_3 Aqueous	LB_PM_3 Solid	LB_PM_3 Aqueous	LB_PM_3 Solid	LB_PM_3 Aqueous	LB_PM_3 Solid	LB_PM_3 Aqueous	LB_PM_3 Solid
Temperature, C	25	25	25	25	25	25	25	25
Pressure, atm	1	1	1	1	1	1	1	1
pH	7.36867	7.93384	7.56551	7.32196	7.32196	7.32196	7.32196	7.32196
Total mol/hr	55.5203	1.96E-04	55.5203	2.92E-08	55.5203	2.92E-08	55.5203	2.92E-08
Flow Units	molality	molality	molality	molality	molality	molality	molality	molality
H2O	55.5087	0.999961	55.5087	0.999961	55.5087	0.999961	55.5087	0.999961
CO2	0.00224	3.03E-07	0.022354	3.03E-06	0.034767	3.03E-06	0.034767	3.03E-06
H2SO4								
H2								
HCL								
HNO3	3.04E-13	1.34E-11	2.43E-11	7.42E-14	3.13E-11	1.10E-14	1.30E-13	1.43E-12
O2								
SiCL4	6.85E-06		8.38E-08					
SO3								
ALOH3	2.40E-09	9.41E-05	7.50E-09	2.40E-09	1.68E-08	2.40E-09	2.91E-08	2.40E-09
KCL	5.29E-09		2.89E-05	5.23E-09	2.70E-05	5.22E-09	2.69E-05	4.49E-09
KHSO4			8.33E-12	8.76E-13	1.42E-12	3.39E-11	5.96E-11	8.07E-12
MGCO3	1.44E-04	4.81E-07	1.55E-04	1.44E-04	3.65E-06	1.55E-04	3.57E-06	1.97E-04
MGH2SiO4	8.69E-10	1.31E-05	1.34E-13	1.34E-13	0.83E-06	1.34E-13	3.20E-06	6.21E-10
NAHCO3	2.30E-05		1.77E-06	2.66E-06	7.34E-06	2.67E-06	1.29E-05	2.62E-06
NAHSO3	6.09E-07		8.24E-04	7.65E-09	3.38E-04	4.73E-09	1.93E-04	5.01E-07
CAH2SiO4	2.81E-10		4.95E-06		4.86E-07		1.58E-07	
CACO3	4.03E-05	0.999906	5.08E-06	0.285735	1.09E-04	5.03E-06	0.511528	0.79E-05
ALCL3								
CAOH2		9.49E-04						
H2CO3								
MGOH2		0.172573			4.31E-04		2.47E-04	
NA2SO4.2H2O	4.49E-04		2.16E-05	4.49E-04	1.00E-04	4.49E-04	1.76E-04	4.44E-04
AL2SO4.3H2O								
AL2SO4.4H2O								
AL2SO4.5H2O								
AL2SO4.6H2O								
AL2SO4.7H2O								
AL2SO4.8H2O								
AL2SO4.9H2O								
AL2SO4.10H2O								
AL2SO4.11H2O								
AL2SO4.12H2O								
AL2SO4.13H2O								
AL2SO4.14H2O								
AL2SO4.15H2O								
AL2SO4.16H2O								
AL2SO4.17H2O								
AL2SO4.18H2O								
AL2SO4.19H2O								
AL2SO4.20H2O								
AL2SO4.21H2O								
AL2SO4.22H2O								
AL2SO4.23H2O								
AL2SO4.24H2O								
AL2SO4.25H2O								
AL2SO4.26H2O								
AL2SO4.27H2O								
AL2SO4.28H2O								
AL2SO4.29H2O								
AL2SO4.30H2O								
AL2SO4.31H2O								
AL2SO4.32H2O								
AL2SO4.33H2O								
AL2SO4.34H2O								
AL2SO4.35H2O								
AL2SO4.36H2O								
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AL2SO4.38H2O								
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AL2SO4.40H2O								
AL2SO4.41H2O								
AL2SO4.42H2O								
AL2SO4.43H2O								
AL2SO4.44H2O								
AL2SO4.45H2O								
AL2SO4.46H2O								
AL2SO4.47H2O								
AL2SO4.48H2O								
AL2SO4.49H2O								
AL2SO4.50H2O								
AL2SO4.51H2O								
AL2SO4.52H2O								
AL2SO4.53H2O								
AL2SO4.54H2O								
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AL2SO4.66H2O								
AL2SO4.67H2O								
AL2SO4.68H2O								
AL2SO4.69H2O								
AL2SO4.70H2O								
AL2SO4.71H2O								
AL2SO4.72H2O								
AL2SO4.73H2O								
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AL2SO4.75H2O								
AL2SO4.76H2O								
AL2SO4.77H2O								
AL2SO4.78H2O								
AL2SO4.79H2O								
AL2SO4.80H2O								
AL2SO4.81H2O								
AL2SO4.82H2O								
AL2SO4.83H2O								
AL2SO4.84H2O								
AL2SO4.85H2O								
AL2SO4.86H2O								
AL2SO4.87H2O								
AL2SO4.88H2O								
AL2SO4.89H2O								
AL2SO4.90H2O								
AL2SO4.91H2O								
AL2SO4.92H2O								
AL2SO4.93H2O								
AL2SO4.94H2O								
AL2SO4.95H2O								
AL2SO4.96H2O								
AL2SO4.97H2O								
AL2SO4.98H2O								
AL2SO4.99H2O								
AL2SO4.100H2O								

Handwritten signature/initials

File: Lb_Waters.xls
 Infiltration: Reconciled 04/21/01, Note Book Page 84
 Additional: SiO2 70.5 mg, AlCl3 9.78E-9 molal, 2.84E-6 mg/L for Al

Case 1	Input CO2 = 0 (molal) = 0 (mg)	logPCO2 = -4.53363	Case 2	Input CO2 = 0.02 (molal) = 880 (mg)	logPCO2 = -3.565348	Case 3	Input CO2 = 0.065 (molal) = 2860 (mg)	logPCO2 = -3.078894
Stream Phase	LB_Infil Aqueous	LB_Infil Solid	LB_Infil Aqueous	LB_Infil Solid	LB_Infil Aqueous	LB_Infil Solid	LB_Infil Aqueous	LB_Infil Solid
Temperature, C	25	25	25	25	25	25	25	25
Pressure, atm	1	1	1	1	1	1	1	1
pH	7.31518	7.93385	7.56551	7.32196	7.32196	7.32196	7.32196	7.32196
Total mol/hr	55.5207	2.50E-04	55.5207	2.50E-04	55.5207	2.50E-04	55.5207	2.50E-04
Flow Units	molality	molality	molality	molality	molality	molality	molality	molality
H2O	55.5087	0.999957	55.5087	0.999957	55.5087	0.999957	55.5087	0.999957
CO2	0.002503	3.29E-07	0.022841	3.06E-06	0.034767	3.06E-06	0.034767	3.06E-06
H2SO4								
H2								
HCL								
HNO3	2.24E-13	8.79E-12	1.40E-11	6.95E-14	3.13E-11	1.10E-14	1.30E-13	1.43E-12
O2								
SiCL4	5.53E-06		8.87E-08					
SO3								
ALOH3	2.40E-09	3.84E-03	8.29E-08	0.000173	2.40E-09	1	8.19E-08	0.000288
KCL	4.49E-09		2.49E-05	4.49E-09	4.49E-09	4.49E-09	4.49E-09	4.49E-09
KHSO4			8.07E-12	6.85E-13	1.42E-12	3.39E-11	5.96E-11	8.07E-12
MGCO3	1.97E-04	5.22E-07	2.10E-04	3.77E-06	1.55E-04	3.77E-06	1.55E-04	3.77E-06
MGH2SiO4	6.21E-10	1.31E-05	1.34E-13	1.34E-13	0.83E-06	1.34E-13	3.20E-06	6.21E-10
NAHCO3	2.30E-05		1.91E-06	2.96E-06	7.34E-06	2.96E-06	1.29E-05	2.62E-06
NAHSO3	5.01E-07		8.19E-04	7.65E-09	3.38E-04	4.94E-09	1.93E-04	5.01E-07
CAH2SiO4	2.81E-10		4.57E-06	5.9E-14	4.86E-07		1.57E-07	
CACO3	4.03E-05	0.99916	5.08E-06	0.285735	1.09E-04	5.03E-06	0.511528	0.79E-05
ALCL3								
CAOH2		9.98E-04						
H2CO3								
MGOH2		0.164707			4.48E-04		2.56E-04	
NA2SO4.2H2O	4.44E-04							

04/23/01

Main species in aqueous

File: Lb_Waters_Main_Species.xls

Phase	Case 1			Case 2			Case 3		
	Aqueous	Solid	Vapor	Aqueous	Solid	Vapor	Aqueous	Solid	Vapor
Temperature, C	90	90	90	90	90	90	90	90	90
Pressure, atm*	0.68715	0.68715	0.68715	0.687288	0.687288	0.687288	0.687867	0.687867	0.687867
Flow Units	molality	molality	molality	molality	molality	molality	molality	molality	molality
Pore Water	logPCo2= -4.53114			logPCo2= -3.561029			logPCo2= -3.074218		
H2O	55.5087		0.999957	55.5087		0.9996	55.5087		0.998775
CO2	3.31E-07		4.28E-05	3.06E-06		4.00E-04	9.40E-06		0.001225
CASO4	0.004021			0.003989			0.003989		
MGSO4	6.55E-04			0.004769			0.004792		
NANO3	0.005269			0.00526			0.005256		
H2SIO3	0.00343			0.003401			0.003402		
SIO2	0.010514	0.248823		0.010429	0.288313		0.010429	0.29103	
KMGCL3	0.006803			0.010244			0.010236		
NA3HSO42	0.00424			0.001998			0.001267		
CACL2	0.023106			0.01473			0.014648		
MGCL2				0.019626			0.019778		
NA2SIO3	0.002407			0.001087			6.22E-04		
NA2SO4	0.004931			0.026629			0.0281		
NACL	0.099242			0.066133			0.065883		
Perm_2	logPCo2= -4.53114			logPCo2= -3.561029			logPCo2= -3.074218		
H2O	55.5087		0.999957	55.5087		0.9996	55.5087		0.998775
CO2	3.31E-07		4.28E-05	3.06E-06		4.00E-04	9.40E-06		0.001225
CASO4	0.004021			0.003989			0.003989		
MGSO4	6.55E-04			0.004769			0.004792		
NANO3	0.005269			0.00526			0.005256		
H2SIO3	0.00343			0.003401			0.003402		
SIO2	0.010514	0.248823		0.010429	0.288313		0.010429	0.29103	
KMGCL3	0.006803			0.010244			0.010236		
NA3HSO42	0.00424			0.001998			0.001267		
CACL2	0.023106			0.01473			0.014648		
MGCL2				0.019626			0.019778		
NA2SIO3	0.002407			0.001087			6.22E-04		
NA2SO4	0.004931			0.026629			0.0281		
NACL	0.099242			0.066133			0.065883		
Perm_3	logPCo2= -4.569164			logPCo2= -3.565249			logPCo2= -3.075581		
H2O	55.5087		0.999961	55.5087		0.999604	55.5087		0.998778
CO2	3.03E-07		3.92E-05	3.03E-06		3.96E-04	9.36E-06		0.001222
CASO4	0.004016			0.003986			0.003986		
MGSO4	6.00E-04			0.004552			0.004574		
NANO3	0.008103			0.008093			0.008086		
H2SIO3	0.003424			0.003396			0.003396		
SIO2	0.010497	0.277016		0.010414	0.318799		0.010414	0.321335	
KMGCL3	0.006952			0.011524			0.011514		
NA3HSO42	0.004223			0.001934			0.001224		
CACL2	0.026033			0.01603			0.01594		
MGCL2				0.019404			0.019552		
NA2SIO3	0.0024			0.001053			6.01E-04		
NA2SO4	0.003036			0.024872			0.026294		
NACL	0.101354			0.068628			0.068398		
Infiltration	logPCo2= -4.533814			logPCo2= -3.561279			logPCo2= -3.074296		
H2O	55.5087		0.999957	55.5087		0.9996	55.5087		0.998775
CO2	3.29E-07		4.28E-05	3.06E-06		4.00E-04	9.40E-06		0.001225
CASO4	0.00402			0.003989			0.003989		
MGSO4	6.51E-04			0.004704			0.004727		
NANO3	0.005266			0.005259			0.005255		
H2SIO3	0.003429			0.003401			0.003401		
SIO2	0.010511	0.249636		0.010427	0.288726		0.010427	0.291412	
KMGCL3	0.006886			0.010242			0.010233		
NA3HSO42	0.004254			0.001997			0.001264		
CACL2	0.02354			0.014961			0.014876		
MGCL2				0.01968			0.019835		
NA2SIO3	0.002395			0.001079			6.17E-04		
NA2SO4	0.004723			0.026145			0.02762		
NACL	0.099566			0.067085			0.066832		

* Pressure slightly different for different water

Note:

In the calculations in Pages 87-90
 I have used mmolal as molal for AlCl3
 the concentration should be 1000 lower than what
 was used for AlCl3.

As the species in page 90 does not
 include Al, the calculation is not changing
 the main species. (it was low).

Recommendation for OLI to change (modify)
 the model Database. see Page 92.

Log, 04/24/01

[Handwritten signature]

Lietai Yang

From: Lietai Yang [ltyang@gargol.cnwra.swri.edu]
Sent: Tuesday, April 24, 2001 10:59 AM
To: 'Support@olisystems.com'
Cc: Roberto Pabalan (rpabalan); Lauren Browning (lbrowning)
Subject: Water Composition

Attention: M. Rafel

Dear Marshall,

The water containing the following species (measured or calculated at about 90oC and 1 atm) is what we want to evaporate. In our preliminary calculations using OLI, temperatures need to be as high as 130oC at 1 atm or 85oC at 40% relative humidity to completely dry this water. Very often, we are outside of the OLI limits (the ionic strength > 30 molal and the water fraction < 0.65). Therefore, we would like OLI to conduct Data Servicing work for the pertinent components so that we can have a reasonable confidence in using the OLI outputs in our analysis.

In our telephone conversation more than a month ago, you have given me a verbal estimate on the cost to do a three salt data servicing. Can you expand the work and cover more salts so that we can better simulate our system? What kind of options are there for our system? Would you please provide a quote for each of the option so that we can make a decision as which option to take?

Also, we have a deadline of late July for this work.

Thanks

Lietai

Concentration for aqueous solution

Table with 2 columns: Component, Molal. Rows include NO3-, Cl-, SO4--, F-, Na+, K+, Ca ++, SiO2 (aq), Mg++, CO2, atm, Li+.

Ref: Presentation by E. Hardin, DC In-Drift Geochemistry Environment And NoteBook #430 page 90

DOE/NRC Tech Exchange, Jan. 9 to 12, 2001
diy. 04/24/01

Continued from page 67.

Calculation for Lead speciation

Objective see page 58.

04/30/01 diy.

File: Darrrell-Pb-chem-2.xls

Results from ESP V6.2e, April 30, 2001. Table with columns for various chemical species and their concentrations across different temperatures and pressures.

Handwritten signatures at the bottom right of the page.

04/30/01

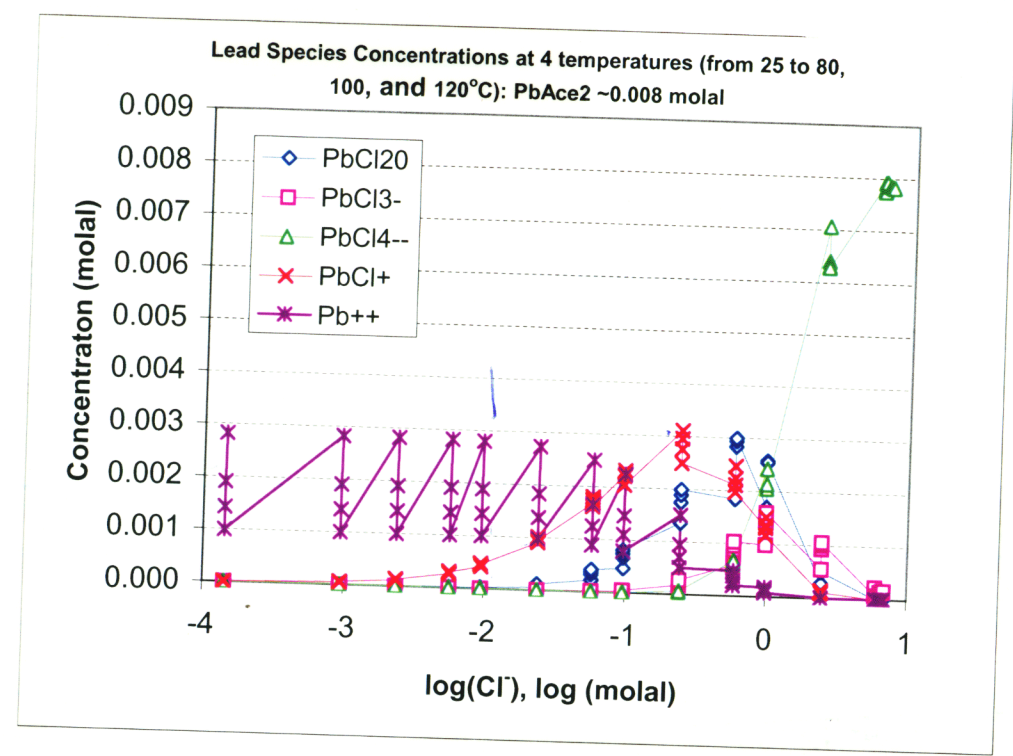
55.514	55.514	55.514	55.514	55.518	55.518	55.518	55.518	55.533	55.533	55.533	55.533	55.568	55.568
-2.24167791	-2.24531613	-2.24552094	-2.2448221	-2.01931139	-2.02279969	-2.0230112	-2.02236247	-1.61990097	-1.62299808	-1.62323696	-1.62279395	-1.23758404	-1.2401479
6.00E-03	6.00E-03	6.00E-03	6.00E-03	1.00E-02	1.00E-02	1.00E-02	1.00E-02	2.50E-02	2.50E-02	2.50E-02	2.50E-02	6.00E-02	6.00E-02
0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008
1652.971679	1652.971679	1652.971679	1652.971679	1652.576168	1652.576168	1652.576168	1652.576168	1651.144027	1651.144027	1651.144027	1651.144027	1647.779236	1647.779236
T25oC	T80oC	T100oC	T120oC	T25oC	T80oC	T100oC	T120oC	T25oC	T80oC	T100oC	T120oC	T25oC	T80oC
Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous
25	80	100	120	25	80	100	120	25	80	100	120	25	80
6.52519	5.80853	5.63669	5.50736	6.53348	5.81964	5.64902	5.52069	6.55996	5.85451	5.68747	5.56221	6.60647	5.91401
55.5299	55.5283	55.5272	55.5262	55.5379	55.5363	55.5353	55.5343	55.5677	55.5662	55.5651	55.5642	55.6373	55.6357
molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality
55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087
1.62E-04	9.13E-04	0.00136542	0.00186848	1.59E-04	8.97E-04	0.00134121	0.00183568	1.51E-04	8.46E-04	0.00126472	0.00173189	1.36E-04	7.58E-04
4.10E-16	5.97E-14	1.97E-13	5.07E-13	3.97E-16	5.77E-14	1.90E-13	4.90E-13	3.57E-16	5.14E-14	1.69E-13	4.37E-13	2.93E-16	4.15E-14
8.84E-16	1.11E-13	4.22E-13	1.28E-12	1.43E-15	1.78E-13	6.75E-13	2.04E-12	3.26E-15	3.95E-13	1.48E-12	4.43E-12	6.70E-15	7.82E-13
3.63E-05	4.25E-05	4.65E-05	5.09E-05	6.01E-05	7.04E-05	7.71E-05	8.44E-05	1.47E-04	1.73E-04	1.91E-04	2.09E-04	3.37E-04	4.04E-04
3.26E-04	7.79E-04	0.00104034	0.00130765	3.13E-04	7.48E-04	0.00100015	0.00125851	2.75E-04	6.56E-04	8.82E-04	0.00111425	2.17E-04	5.15E-04
4.11E-06	6.92E-06	8.31E-06	9.75E-06	1.07E-05	1.77E-05	2.11E-05	2.46E-05	5.49E-05	8.65E-05	1.01E-04	1.15E-04	2.21E-04	3.32E-04
1.88E-07	1.64E-06	2.75E-06	4.27E-06	1.86E-07	1.63E-06	2.74E-06	4.25E-06	1.81E-07	1.60E-06	2.70E-06	4.21E-06	1.72E-07	1.54E-06
3.93E-08	1.85E-07	2.77E-07	4.01E-07	4.05E-08	1.92E-07	2.90E-07	4.20E-07	4.43E-08	2.16E-07	3.30E-07	4.84E-07	5.13E-08	2.61E-07
0.00573221	0.00568439	0.00568171	0.00569086	0.00956508	0.00948856	0.00948394	0.00949768	0.0239938	0.0238233	0.0238102	0.0238345	0.057865	0.0575244
3.42E-07	1.79E-06	2.67E-06	3.60E-06	3.38E-07	1.77E-06	2.63E-06	3.54E-06	3.27E-07	1.69E-06	2.50E-06	3.36E-06	3.05E-07	1.54E-06
8.05E-12	1.36E-10	2.64E-10	4.66E-10	8.23E-12	1.41E-10	2.75E-10	4.86E-10	8.80E-12	1.56E-10	3.09E-10	5.55E-10	9.84E-12	1.84E-10
0.00596461	0.00595857	0.00595461	0.00595029	0.00994151	0.00993134	0.00992467	0.00991744	0.0248575	0.0248311	0.024814	0.0247953	0.059672	0.0596065
0.0101893	0.00857838	0.00756793	0.00652081	0.0103385	0.00876975	0.00776914	0.00672219	0.0107813	0.00933947	0.00836998	0.00732612	0.0114483	0.0102112
2.62E-04	4.05E-04	5.42E-04	7.10E-04	2.56E-04	3.98E-04	5.36E-04	7.06E-04	2.36E-04	3.75E-04	5.13E-04	6.87E-04	2.01E-04	3.28E-04
0.0041755	0.00369698	0.00331745	0.00281738	0.00404944	0.00357527	0.00320787	0.00272538	0.00366398	0.00320575	0.0028757	0.00244587	0.00304314	0.00261732
1.15E-08	1.85E-08	2.33E-08	2.92E-08	4.08E-08	7.93E-08	9.88E-08	1.23E-07	6.38E-07	9.75E-07	1.19E-06	1.45E-06	6.32E-06	9.08E-06
5.49E-11	5.14E-11	6.04E-11	7.42E-11	4.08E-10	3.78E-10	4.42E-10	5.41E-10	1.41E-08	1.27E-08	1.47E-08	1.77E-08	3.80E-07	3.26E-07
2.61E-04	3.03E-04	3.03E-04	2.91E-04	4.15E-04	4.77E-04	4.75E-04	4.55E-04	9.00E-04	0.00100495	9.88E-04	9.35E-04	0.00168117	0.00179408
0.00281045	0.0018981	0.00142593	9.99E-04	0.00279706	0.00188783	0.00142032	9.99E-04	0.00272003	0.00182573	0.0013763	9.72E-04	0.00249431	0.00164909
1.62E-04	9.12E-04	0.0013623	0.00186313	1.59E-04	8.95E-04	0.00133806	0.0018303	1.51E-04	8.44E-04	0.00126149	0.00172636	1.36E-04	7.56E-04
1002.8	1002.8	1002.8	1002.8	1003.04	1003.04	1003.04	1003.04	1003.91	1003.91	1003.91	1003.91	1005.96	1005.96
0.00100367	0.00102925	0.00104378	0.00106102	0.00100374	0.00102932	0.00104385	0.00106108	0.00100399	0.00102996	0.00104411	0.00106132	0.00100459	0.00103026
-3.79E+06	-3.74E+06	-3.72E+06	-3.70E+06	-3.70E+06	-3.74E+06	-3.72E+06	-3.70E+06	-3.80E+06	-3.74E+06	-3.72E+06	-3.70E+06	-3.80E+06	-3.74E+06
9.99E+05	9.74E+05	9.61E+05	9.45E+05	9.99E+05	9.74E+05	9.61E+05	9.45E+05	1.00E+06	9.75E+05	9.62E+05	9.46E+05	1.00E+06	9.76E+05
0.591689	0.663697	0.681658	0.699889	0.746739	0.845622	0.873428	0.901401	1.3861	1.58986	1.65239	1.71151	2.95386	3.39164
0.00151937	0.00285785	0.00303123	0.00336031	0.00195976	0.00383421	0.00421174	0.00474246	0.00356306	0.00736989	0.00847795	0.00972613	0.00713674	0.0151858
108.925	207.7	212.159	232.042	109.283	217.334	232.652	260.181	108.403	228.893	261.535	301.261	105.434	229.617
0.896983	0.356674	0.283563	0.233593	0.897279	0.356846	0.2837	0.233711	0.898428	0.357513	0.284245	0.234174	0.901114	0.359066
1.00703	1.00704	1.00705	1.00699	1.00736	1.00752	1.0074	1.0074	1.00865	1.0094	1.00947	1.0094	1.01167	1.01379
0.018942	0.0165659	0.0152175	0.0139207	0.0229568	0.0205447	0.0192095	0.0179241	0.0377322	0.035365	0.0340709	0.0328215	0.0720162	0.0697226

Jagers stude

55.568	55.568	55.608	55.608	55.608	55.608	55.608	55.608	55.608	55.608	55.608	55.608	55.608	55.608
-1.24043187	-1.24021208	-1.01425342	-1.01642242	-1.01672427	-1.0166322	-0.61351174	-0.61476205	-0.61505729	-0.61516291	-0.2318527	56.108	56.108	56.108
6.00E-02	6.00E-02	1.00E-01	1.00E-01	1.00E-01	1.00E-01	2.50E-01	2.50E-01	2.50E-01	2.50E-01	6.00E-01	6.00E-01	6.00E-01	6.00E-01
0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008
1647.779236	1647.779236	1643.955172	1643.955172	1643.955172	1643.955172	1629.795686	1629.795686	1629.795686	1629.795686	1598.42626	0.008	0.008	0.008
T100oC	T120oC	T25oC	T80oC	T100oC	T120oC	T25oC	T80oC	T100oC	T120oC	T25oC	T80oC	T100oC	T120oC
Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous
100	120	25	80	100	120	25	80	100	120	25	80	100	120
5.75241	5.63199	6.64697	5.96425	5.80664	5.68962	6.75453	6.09086	5.94094	5.83106	6.9928	5.7054	6.27985	6.13613
55.6348	55.6337	55.7167	55.7151	55.7142	55.7132	56.0141	56.0126	56.0118	56.0109	56.7054	56.7054	56.7054	56.7054
molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality
55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087
0.00113233	0.00155223	1.24E-04	6.82E-04	0.00101984	0.00139969	9.28E-05	5.00E-04	7.46E-04	0.00102774	4.77E-05	55.5087	55.5087	55.5087
1.37E-13	3.53E-13	2.43E-16	3.39E-14	1.12E-13	2.90E-13	1.41E-16	1.87E-14	6.16E-14	1.61E-13	4.77E-05	55.5087	55.5087	55.5087
2.89E-12	8.48E-12	9.79E-15	1.11E-12	4.05E-12	1.18E-11	1.74E-14	1.88E-12	6.68E-12	1.90E-11	2.14E-14	2.55E-12	8.88E-12	2.47E-11
4.48E-04	4.96E-04	5.42E-04	6.54E-04	7.30E-04	8.13E-04	0.00121591	0.0014784	0.00166875	0.00188166	0.00244844	0.00290199	0.00328114	0.00372185
6.97E-04	8.89E-04	1.74E-04	4.09E-04	5.57E-04	7.17E-04	9.06E-05	2.05E-04	3.69E-04	0.00188166	0.00244844	0.00290199	0.00328114	0.00372185
3.78E-04	4.20E-04	4.50E-04	6.56E-04	7.34E-04	8.02E-04	0.00135117	0.00174409	0.00188109	0.00198776	0.00182986	0.0028301	0.00293603	0.00298835
2.62E-06	4.12E-06	1.65E-07	1.49E-06	2.54E-06	4.02E-06	1.44E-07	1.30E-06	2.26E-06	3.61E-06	1.12E-07	1.76E-07	1.20E-06	1.92E-06
4.06E-07	6.07E-07	5.79E-08	3.04E-07	4.80E-07	7.76E-08	4.38E-07	7.11E-07	1.11E-06	1.36E-07	0.586337	0.586947	0.58667	0.586367
0.0574668	0.0575159	0.0967713	0.0962892	0.0962223	0.0962427	0.243494	0.242794	0.242629	0.24257	0.586337	0.586947	0.58667	0.586367
2.26E-06	3.02E-06	2.85E-07	1.42E-06	2.06E-06	2.74E-06	2.30E-07	1.11E-06	1.60E-06	2.11E-06	1.32E-07	7.25E-07	1.04E-06	1.35E-06
3.73E-10	6.85E-10	1.08E-11	2.08E-10	4.31E-10	8.05E-10	1.32E-11	2.72E-10	5.82E-10	1.13E-09	2.00E-11	3.64E-10	7.96E-10	1.58E-09
0.0595626	0.0595154	0.0994738	0.0993631	0.0992875	0.0992056	0.248823	0.248563	0.248374	0.248162	0.597645	0.597195	0.596817	0.596379
0.00930329	0.00828086	0.011917	0.0108379	0.00999034	0.00900275	0.0126725	0.0118794	0.0					

Pb 2-ly. 04/30/01

File: Darrel_Pt-Chem-2.XLS



J. Yang
8/14/02

05/07/01

Using HCl as Cl⁻ source

2-ly. 05/07/01

File: Darrel_Darrel-Chem-3.XLS

Results from ESP V6.2b, May 07, 2001
Pb MW = 207.2 mg/l (appr. ppm)

Inputs	1	100	1600	2100	Not Right, Organic shown				
log/free Cl-	0.004826255	0.482625483	7.722007722	10.1351351					
H2O (mol)	55.5	55.5	55.5	55.5	55.5105	55.5	55.5	55.5	55.5
NaCl (mol)	-3.84912081	-3.84912081	-3.84912081	-3.84912081	-2.63339216	-2.63339216	-2.63339216	-2.63339216	-2.63339216
LiCl (mol)	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5
HCl (mol)	1.50E-04	1.50E-04	1.50E-04	1.50E-04	1.50E-04	1.50E-04	1.50E-04	1.50E-04	1.50E-04
PbCl2 (mol)	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03
Pb(CH3CO2)2 (mol)	0.008	0.008	0.008	0.008	2.50E-03	2.50E-03	2.50E-03	2.50E-03	2.50E-03
PbSO4 (mol)	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008
Total Pb (ppm)	1653.53231	1653.53231	1653.53231	1653.53231	1653.482828	1653.482828	1653.482828	1653.482828	1653.482828

Stream	25°C	80°C	100°C	250°C	80°C	100°C	250°C	80°C	100°C	250°C	80°C	100°C
Phase	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous
Temperature, C	25	80	100	25	80	100	25	80	100	25	80	100
Pressure, atm	1	1	1	1	1	1	1	1	1	1	1	1
pH	6.31747	5.7487	5.585	5.69171	5.53244	5.421	5.25263	5.22865	5.17119	4.26961	4.29633	4.28398
Total mol/hr	55.5181	55.5165	55.5155	55.5192	55.5176	55.5166	55.5211	55.5197	55.5187	55.5307	55.5297	55.5292
Flow Units	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality
H2O	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087
ACETIC ACID	2.58E-04	0.00102201	0.00149034	0.00102468	0.00157784	0.00202571	0.00250455	0.00281922	0.00317107	0.00994188	0.0100031	0.0100932
ACET2	1.03E-15	7.47E-14	2.34E-13	1.64E-14	1.78E-13	4.33E-13	9.78E-14	5.69E-13	1.06E-12	1.54E-12	7.16E-12	1.07E-11
H2SO4	3.63E-17	3.25E-15	1.22E-14	1.02E-15	3.54E-14	1.17E-13	6.96E-15	1.78E-13	5.14E-13	2.59E-13	5.68E-12	1.47E-11
HCl												
LiOH												
LiOAc												
LiOAc2												
PbCl2	3.47E-04	8.31E-04	0.00111009	3.22E-04	8.00E-04	0.0010764	2.73E-04	7.09E-04	9.74E-04	6.49E-05	1.88E-04	2.81E-04
PbCl3-	2.91E-09	5.07E-09	6.20E-09	1.35E-07	2.42E-07	3.02E-07	8.89E-07	1.66E-06	2.13E-06	1.85E-05	3.66E-05	4.96E-05
PbCl4--	7.92E-08	1.40E-06	2.47E-06	4.65E-09	5.65E-07	1.30E-06	6.58E-10	1.57E-07	4.79E-07	9.91E-12	3.30E-09	1.36E-08
PbCl+	2.39E-08	1.57E-07	2.40E-07	5.67E-09	9.57E-08	1.65E-07	2.07E-09	4.78E-08	9.31E-08	2.19E-10	5.70E-09	1.23E-08
Pb++	1.43E-04	1.42E-04	1.41E-04	9.50E-04	9.38E-04	9.36E-04	0.0023665	0.00232599	0.00231343	0.00924424	0.00891535	0.00873341
LiOH	5.41E-07	2.01E-06	2.52E-06	2.29E-06	3.31E-06	4.28E-06	6.30E-06	6.69E-06	7.63E-06	6.12E-05	5.81E-05	6.00E-05
LiOAc	2.06E-12	8.98E-11	2.05E-10	2.87E-14	2.43E-11	7.38E-11	1.48E-15	3.36E-12	1.54E-11	2.34E-18	8.40E-15	5.78E-14

Inputs	1	100	1600	2100
PbAce3	0.00983352	0.0081498	0.00712146	0.009271
PbAce+	2.68E-04	4.09E-04	5.42E-04	2.35E-04
PbCl3-	0.00441159	3.38E-13	0.00394066	0.00354478
PbCl4--	2.03E-13	4.32E-13	6.23E-11	1.07E-10
PbCl+	2.31E-17	2.21E-17	2.63E-17	4.98E-05
Pb++	1.72E-06	8.47E-06	8.57E-06	6.14E-05
PbOH+	0.00285882	0.00193931	0.00145543	0.00301021
PbOH2	1.08E-04	8.71E-04	0.00133805	2.68E-05

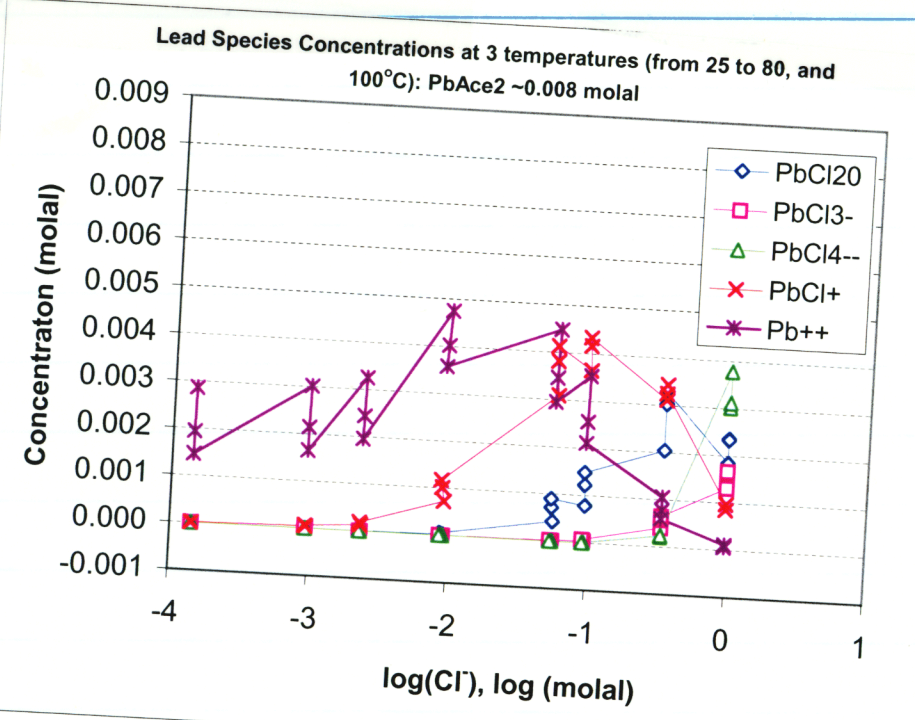
J. Yang
8/14/02

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55.568	-1.2514035	-1.2618484	-1.2675411	55.608	-1.0237413	-1.0304616	-1.033932	55.858	-0.4703748	-0.4710319	-0.4719064	56.508	-0.010338	-0.0098188	-0.0100157
55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5
6.00E-02	6.00E-02	6.00E-02	6.00E-02	1.00E-01	1.00E-01	1.00E-01	1.00E-01	3.50E-01	3.50E-01	3.50E-01	3.50E-01	1.00E+00	1.00E+00	1.00E+00	1.00E+00
0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008
1649.94426	1649.94426	1649.94426	1647.54995	1647.54995	1647.54995	1647.54995	1647.54995	1633.28045	1633.28045	#REF!	#REF!	1595.51838	1595.51838	1595.51838	1595.51838

T25oC	T80oC	T100oC	T25oC	T80oC	T100oC	T25oC	T80oC	T100oC	T25oC	T80oC	T100oC	T25oC	T80oC	T100oC
Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous
25	80	100	25	80	100	25	80	100	25	80	100	25	80	100
1	1	1	1	1	1	1	1	1	1	1	1	1	1	1
1.44218	1.45217	1.45657	1.17321	1.18612	1.19189	0.593389	0.615492	0.624962	0.0966449	0.130527	0.143912	55.5241	55.6227	55.622
molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality
55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087
0.0159891	0.0159891	0.0159891	0.0159891	0.0159891	0.0159891	0.0159891	0.0159891	0.0159891	0.0159891	0.0159891	0.0159891	0.0159891	0.0159891	0.0159891
3.99E-12	1.83E-11	2.70E-11	4.00E-12	1.83E-11	2.70E-11	4.02E-12	1.84E-11	2.72E-11	4.07E-12	1.87E-11	2.75E-11	8.84E-10	2.24E-08	5.58E-08
molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality
2.60E-10	5.97E-10	8.82E-10	5.23E-11	1.12E-10	1.59E-10	8.22E-13	1.75E-12	2.28E-12	8.11E-15	1.66E-14	2.03E-14	4.16E-04	7.10E-04	8.97E-04
molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality
1.53E-17	4.09E-15	1.70E-14	3.07E-18	7.62E-16	3.04E-15	4.74E-20	1.17E-17	4.29E-17	4.45E-22	1.06E-19	3.64E-19	3.57E-13	9.06E-12	2.06E-11
molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality
0.0560527	0.0547207	0.0540081	0.0496801	0.0492283	0.04924843	0.338396	0.33804	0.33736	0.976477	0.977645	0.977202	0.0440203	0.0440183	0.0440175
molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality
5.84E-27	1.64E-23	1.19E-22	6.55E-28	1.73E-24	1.22E-23	2.94E-30	8.04E-27	5.27E-26	0.984154	0.984147	0.984136	8.97E-06	7.25E-06	6.47E-06
molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality
1.84E-13	2.62E-13	3.92E-13	2.07E-14	2.78E-14	4.03E-14	9.57E-17	1.33E-16	1.80E-16	3.27E-19	4.57E-19	5.91E-19	4.48E-06	4.10E-06	4.09E-06
molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality
1.71E-05	1.88E-05	2.46E-05	3.78E-05	5.65E-05	7.11E-05	3.98E-04	5.67E-04	6.45E-04	0.00130757	0.00159759	0.00165685	6.71E-07	6.34E-07	7.78E-07
molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality
0.00308755	0.00381001	0.00413013	0.00365048	0.00416271	0.0043371	0.00319832	0.00343018	0.00324283	9.71E-04	9.68E-04	8.45E-04	0.00448115	0.00345778	0.00294443
molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality
1.73E-09	5.67E-08	1.41E-07	6.68E-10	2.04E-08	4.87E-08	4.35E-11	1.32E-09	2.89E-09	1.38E-12	3.97E-11	8.18E-11	0.00100428	0.00102995	0.00104453
molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality
-3.80E+06	-3.74E+06	-3.72E+06	-3.80E+06	-3.74E+06	-3.72E+06	-3.81E+06	-3.75E+06	-3.73E+06	-3.83E+06	-3.78E+06	-3.76E+06	1.00E+06	9.75E+05	9.62E+05
molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality
2.79267	3.18697	3.3024	4.61178	5.26491	5.45671	16.3361	18.6238	19.2792	50.5164	57.1693	59.1302	0.0187763	0.0318795	0.0353741
molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality
0.895419	0.357043	0.283954	0.897696	0.358523	0.28519	0.911567	0.367656	0.292802	0.946289	0.390301	0.311688	0.0605565	0.0562064	0.056986
molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality
0.0605565	0.0562064	0.056986	0.0982648	0.0958536	0.0946778	0.340551	0.34002	0.339308	0.989227	0.988352	0.988259	0.0100428	0.00102995	0.00104453
molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality



05/07/01

05/07/01

Log.

Changing Pb Concentration

05/1/01

Inputs	HCl or NaCl 0.01 molal, varying Pb											
	55.518	-2.0341288	-2.0498616	-2.0588162	55.526	-2.0371767	-2.050764708	-2.0576253	55.534	-2.039691	-2.0531662	55.538
log(free Cl-)	-2.0341288	-2.0498616	-2.0588162	55.526	-2.0371767	-2.050764708	-2.0576253	55.534	-2.039691	-2.0531662	55.538	-2.0193114
H2O (mol)	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5
NaCl (mol)	1.00E-02	1.00E-02	1.00E-02	1.00E-02	1.00E-02	1.00E-02	1.00E-02	1.00E-02	1.00E-02	1.00E-02	1.00E-02	1.00E-02
HCl (mol)	0.008	0.008	0.008	0.016	0.016	0.016	0.016	0.024	0.024	0.024	0.024	0.008
Pb(CH3CO2)2	0.008	0.008	0.008	0.016	0.016	0.016	0.016	0.024	0.024	0.024	0.024	0.008
PbSO4 (mol)	0.008	0.008	0.008	0.016	0.016	0.016	0.016	0.024	0.024	0.024	0.024	0.008
Total Pb (mol)	1652.93871	1652.93871	1652.93871	3297.32848	3297.32848	3297.32848	3297.32848	4933.23545	4933.23545	4933.23545	4933.23545	1652.93871

Inputs	HCl or NaCl 0.001 molal, Varying Pb											
	55.509	-3.027649	-3.028627	55.517	-3.027862	-3.0339757	-3.0353068	55.525	-3.0349207	-3.0428335	55.538	-3.0269064
log(free Cl-)	55.509	-3.027649	-3.028627	55.517	-3.027862	-3.0339757	-3.0353068	55.525	-3.0349207	-3.0428335	55.538	-3.0269064
H2O (mol)	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5
NaCl (mol)	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03
HCl (mol)	0.008	0.008	0.008	0.016	0.016	0.016	0.016	0.024	0.024	0.024	0.024	0.008
Pb(CH3CO2)2	0.008	0.008	0.008	0.016	0.016	0.016	0.016	0.024	0.024	0.024	0.024	0.008
PbSO4 (mol)	0.008	0.008	0.008	0.016	0.016	0.016	0.016	0.024	0.024	0.024	0.024	0.008
Total Pb (mol)	1653.48283	1653.48283	1653.48283	3298.41109	3298.41109	3298.41109	3298.41109	4933.26436	4933.26436	4933.26436	4933.26436	1653.48283

J. Yang

3/11/02

05/07/01

May 10/01

Lietai Yang

To: Yi-ming Pan (ypan)
Cc: Darrell Dunn (ddunn); Gustavo Cragolino; Vijay Jain (vjain)
Subject: RE: Pb speciations

Enclosed are the results of more calculations.

It seems that Pb Acetate does not decociate easily (only ~30%). If Cl- is not abosolutely required, then just add PbCl2 alone (not adding other chlorides in order to maintain low Cl- conc) would allow you to achieve 3000 ppm Pb++ (with only a small percentage of Cl complex). A slight amount of HCl helps only slightly for Pb++. If too much HCl, then the Cl- is too much and complex will be formed.

It is an interesting try with the PbSO4. If nothing else is added, the Pb is dissociated into Pb++ almost completely at T> 80oC. Is SO4-- bad for the test?

Regards.

Lietai



Darrell_Pb_Chem_4.xls

Handwritten signature 'Lietai Yang' and date '2/10/02'.

File: Darrell-Pb-chem_4 05/10/01.xls

Table with columns for various chemical species and rows for different temperatures (T25oC, T80oC, T100oC) and phases (Aqueous, Solid). Includes species like PbSO4, PbCl2, PbAc2, and various ions.

Handwritten signature 'Lietai Yang' and date '2/10/02'.

05/10/01

soluble above 40°C ---->																				
PbSO4 + HCl, still not soluble at 25°C					PbSO4 only, 50, 65 °C					PbSO4 only, 30, 35, 40 °C					PbSO4 only, 50, 65 °C					
#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	
55.525	55.525	55.525	55.525	55.525	55.525	55.525	55.525	55.525	55.525	55.525	55.525	55.525	55.525	55.525	55.525	55.525	55.525	55.525	55.525	
0.87675	0.87675	0.87675	0.87675	0.87675	0.87675	0.87675	0.87675	0.87675	0.87675	0.87675	0.87675	0.87675	0.87675	0.87675	0.87675	0.87675	0.87675	0.87675	0.87675	
55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	
1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	1.00E-03	
0.024	0.024	0.024	0.024	0.024	0.024	0.024	0.024	0.024	0.024	0.024	0.024	0.024	0.024	0.024	0.024	0.024	0.024	0.024	0.024	
4973.11828	4973.11828	4973.11828	4973.11828	4973.11828	4973.11828	4973.11828	4973.11828	4973.11828	4973.11828	4973.11828	4973.11828	4973.11828	4973.11828	4973.11828	4973.11828	4973.11828	4973.11828	4973.11828	4973.11828	
T25oC	T25oC	T80oC	T100oC	ec	T25oC	T50oC	T65oC	T30oC	T35oC	T40oC	T40oC	T43oC	T45oC	T47.5oC	T25oC	T50oC	T65oC	T30oC	T35oC	
Aqueous	Solid	Aqueous	Aqueous	Aqueous	Solid	Aqueous	Aqueous	Solid	Solid	Aqueous	Solid	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	
25	25	80	100	1	25	50	65	30	35	40	40	43	45	47.5	25	50	65	30	35	
1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	
3.02476	3.02476	3.72665	3.88385	5.73849	4.6521	4.50222	5.83615	5.53815	5.53815	5.44433	4.73382	4.70967	4.68039	4.68039	5.55023	5.5489	5.5489	5.55003	5.55003	
55.5023	55.5023	55.5489	55.5487	55.5003	0.0238516	55.5479	55.5479	55.5003	0.0238277	55.5004	0.0238157	55.5479	55.5479	55.5479	55.5087	55.5087	55.5087	55.5087	55.5087	
molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	
55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	55.5087	
4.23E-19	5.33E-13	5.47E-23	3.53E-18	3.15E-18	1.64E-24	2.26E-20	6.70E-20	3.14E-24	5.92E-24	1.10E-23	1.31E-20	1.53E-20	1.86E-20	1.86E-20	1.55E-12	1.28E-21	1.87E-21	4.29E-24	1.71E-23	
1.23E-08	1.55E-15	1.23E-08	5.60E-07	7.34E-07	4.01E-10	2.75E-09	6.18E-09	5.14E-10	6.51E-10	8.14E-10	1.87E-09	2.09E-09	2.40E-09	2.40E-09	6.67E-10	6.43E-09	6.43E-09	4.01E-10	1.71E-13	
1.12E-11	9.96E-04	9.88E-04	1.86E-09	5.94E-09	5.71E-09	3.37E-09	5.43E-09	6.32E-09	7.39E-09	8.31E-09	2.66E-09	2.85E-09	3.10E-09	3.10E-09	2.97E-05	2.51E-04	1.77E-04	2.97E-05	4.21E-05	
1.92E-23	1.20E-05	1.20E-05	5.23E-16	1.25E-14	2.52E-15	3.93E-05	8.73E-05	3.72E-08	5.78E-08	8.87E-08	2.65E-05	2.97E-05	3.42E-05	3.42E-05	6.05E-15	5.23E-16	1.25E-14	6.05E-15	1.74E-14	
5.96E-12	4.06E-15	3.72E-06	1.99E-10	2.56E-10	1.02E-13	1.17E-13	2.47E-04	2.94E-04	0.0239348	0.0239493	1.47E-04	0.0239493	1.47E-04	1.62E-04	3.86E-09	1.54E-04	1.62E-04	3.86E-09		
1.62E-04	3.86E-09	1.54E-04	0.0239348	0.0239493	1.47E-04	0.0239493	1.47E-04	0.0239493	1.47E-04	0.0239493	1.47E-04	0.0239493	1.47E-04	0.0239493	1.47E-04	0.0239493	1.47E-04	0.0239493	1.47E-04	0.0239493
999.936	7.22796	1007.16	1007.16	999.894	7.23332	1007.13	1007.13	999.898	7.22971	999.901	7.22608	999.905	7.22245	1007.13	1007.13	1007.13	1007.13	1007.13	1007.13	
0.00100303	1.14E-05	0.0102897	0.0104315	0.0100301	1.14E-06	0.0010209	0.00101959	0.00100446	1.14E-06	0.00100609	1.14E-06	0.00100789	1.14E-06	0.00100912	0.00100993	0.00101099	0.00101099	0.00101099	0.00101099	
-3.79E+06	-5240.35	-3.74E+06	-3.72E+06	-3.79E+06	-5244.25	-3.77E+06	-3.76E+06	-3.79E+06	-5238.65	-3.78E+06	-5233.05	-3.78E+06	-5227.45	-3.78E+06	-3.78E+06	-3.77E+06	-3.77E+06	-3.77E+06	-3.77E+06	
9.97E+05	6.32E+06	9.97E+05	9.97E+05	9.97E+05	6.32E+06	9.95E+05	9.88E+05	9.95E+05	6.32E+06	9.95E+05	6.32E+06	9.95E+05	6.32E+06	9.95E+05	6.32E+06	9.95E+05	6.32E+06	9.95E+05	6.32E+06	
0.0505751	0.827987	0.842271	0.00694981	0.769715	0.790557	0.00760471	0.00827393	0.0085932	0.758797	0.761988	0.765897	0.765897	0.765897	0.765897	0.765897	0.765897	0.765897	0.765897	0.765897	
4.57E-04	0.0125842	0.0151223	4.35E-05	0.00849462	0.0104305	5.21E-05	6.16E-05	7.21E-05	0.00761246	0.00786243	0.00817726	0.00817726	0.00817726	0.00817726	0.00817726	0.00817726	0.00817726	0.00817726	0.00817726	
18.3239	521.293	657.28	1.81708	358.221	443.115	2.18038	2.58423	3.02944	320.078	330.855	344.463	344.463	344.463	344.463	344.463	344.463	344.463	344.463	344.463	
0.89098	0.359815	0.286131	0.890996	0.55557	0.440112	0.798339	0.720282	0.653849	0.627616	0.605544	0.57968	0.57968	0.57968	0.57968	0.57968	0.57968	0.57968	0.57968	0.57968	
1.00029	1.0159	1.01617	1.00031	1.01526	1.01579	1.00033	1.00037	1.00037	1.01494	1.01504	1.01515	1.01515	1.01515	1.01515	1.01515	1.01515	1.01515	1.01515	1.01515	
0.00163319	0.0948638	0.0941309	5.92E-04	0.0958675	0.0957112	6.39E-04	6.86E-04	7.33E-04	0.095911	0.0959	0.0958847	0.0958847	0.0958847	0.0958847	0.0958847	0.0958847	0.0958847	0.0958847	0.0958847	

J. Yang Zhang

05/10/01

Pb Acetate only, ~20% dissociation										Low PbCl2 only, ~70% dissociation					High PbCl2, ~50% dissociation					High PbCl2 + HCl, ~40% dissociation					High PbCl2 + HCl, ~50% dissociation				
#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!	#VALUE!
55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508	55.508
log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)	log(free Cl)
35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255	35.2255
80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795	80.795
55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5	55.5
0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008
0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008	0.008
1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881	1653.54881
Stream	T25oC	T80oC	T100oC	T25oC	T80oC	T100oC	T25oC	T80oC	T100oC	T25oC	T80oC	T100oC	T25oC	T80oC	T100oC	T25oC	T80oC	T100oC	T25oC	T80oC	T100oC	T25oC	T80oC	T100oC	T25oC	T80oC	T100oC	T25oC	T80oC
Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous	Aqueous
25	80	100	25	80	100	25	80	100	25	80	100	25	80	100	25	80	100	25	80	100	25	80	100	25	80	100	25	80	100
1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1
55.5179	55.5163	55.5152	55.5224	55.5216	55.5212	55.563	55.5598	55.5581	55.608	55.6043	55.6023	3.08643	3.08946	3.0856	0.0398302	0.036371	0.0348849	0.0398302	0.036371	0.0348849	0.0398302	0.036371	0.0348849	0.0398302	0.036371	0.0348849	0.0398302	0.036371	0.0348849
molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality	molality												

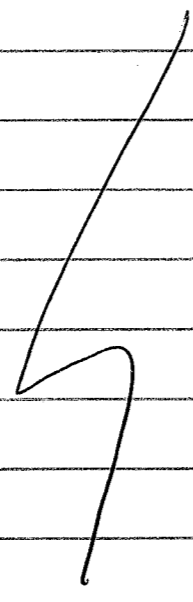
Below 40°C , solid PbSO_4 forms, but above 45°C , no solid forms.

Called OLI, found out that they only have data to 40°C . Above 40°C , the software assumed a infinity solubility for PbSO_4 .

I should not rely on the results for $T > 40^{\circ}\text{C}$

J. Yang

05/11/01


J. Yang
3/14/02

May 11/01

OLI Contacted. There is no data for PbSO_4 above 40°C . The solubility was assumed infinity at $T > 40^{\circ}\text{C}$.

Lietai Yang

From: Jim Berthold [Support@olisystems.com]
Sent: Friday, May 11, 2001 10:47 AM
To: Yang Lietai
Subject: PbSO4



pbs04.zip



Databook Tour.PDF



OLI Tips 2 Load
DataBase.doc

Lietai,

Attached are several files. The first is the revised lead sulfate database. I extended the applicable temperature range to 100 C. Be advised, we make no guarantee above 40 C. The data is from Seidell. The compressed file is PBSO4.ZIP and contains the OLI/ESP database PBSO4. This is an ESP type database.

The second file is a tour of the OLI/Databook. You should review this since it will help you determine the contents of the database I just provided.

The final file is instructions for importing the database into the OLI/Analyzers. You can not use the ESP format database directly.

To use this database decompress the zip file into the following folder:

c:\oli65\esp

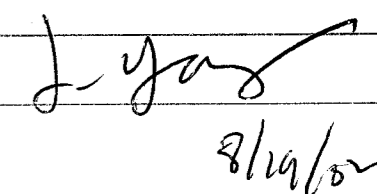
This assumes you have OLI65 installed. If you are still using oli62, then install in \oli62\esp

When decompressed, there will be approximately 39 files.

Take the tour to see how to generate a model with a private database. When you do this for real, substitute PBSO4 for GEOCHEM as explained in the tour.

Give me a call if you have questions.

Jim Berthold
OLI Systems, Inc.
Customer Relations
support@olisystems.com
www.olisystems.com
(973) 539-4996 extension 24
(973) 539-5922 FAX


J. Yang
3/14/02

SOLUBILITIES

INORGANIC AND METAL-ORGANIC COMPOUNDS

K - Z

*A Compilation of Solubility Data
from the Periodical Literature*

VOLUME II FOURTH EDITION

by
William F. Linke, Ph.D.
American Cyanamid Co., Stamford, Conn.

**A Revision and Continuation of the Compilation
Originated by
Arthurton Seidell, Ph.D.
U. S. National Institutes of Health**

1965

American Chemical Society
Washington, D.C.

*L. Yang
3/10/12*

LEAD

LEAD SULFATE PbSO₄

SOLUBILITY IN WATER

(Average curve from gravimetric results of Dibbitts (1874), Beck and Stegmüller (1910) and Pleissner (1907) and conductivity results of Böttger (1903) and Kohlrausch (1904-05).)

t°	Gms. PbSO ₄ per Liter	t°	Gms. PbSO ₄ per Liter
0	0.028	20	0.041
5	0.031	25	0.045
10	0.035	30	0.049
15	0.038	35	0.052
18	0.040	40	0.056

Later determinations of the solubility of lead sulfate in water by Crookford and Brawley, 1934; Purdum and Rutherford, 1933; Kolthoff and Rosenblum, 1933; and Huybrechts and de Langeron, 1930, gave an average curve from which the following values were taken.

t°	Gms. PbSO ₄ per Liter	t°	Gms. PbSO ₄ per liter
0	0.0330	25	0.0452 <i>Wed</i>
5	0.0354	30	0.0476 <i>Thu</i>
10	0.0380	35	0.0500
15	0.0403	40	0.0526
20	0.0427	50	0.0574 <i>Aug. 05/14/01</i>

Koizumi, 1950 reports that the effect of dissolved CO₂ on the solubility of PbSO₄ is negligible.

SOLUBILITY OF LEAD SULFATE IN SULFURIC ACID SOLUTIONS

Results of Crookford and Brawley, 1936; Crookford and Addressstone, 1936

In agreement with Donk, 1916, analyses of the solid phases showed that PbSO₄ is the only one at these temperatures. The eutectic temperature for PbSO₄ + H₂SO₄ was found to be 5.4°. The acid concentration of 104 percent H₂SO₄ corresponds to 80.5 percent SO₃.

Gms. H ₂ SO ₄ per 1000 gms. aq. solvent	0°	25°	35°	50°
0.0	0.033	0.0445	0.0497	0.0577
0.05	0.008	0.0100	0.0110	0.0240
0.1	0.007	0.0080	0.0100	0.0210
0.2	0.0064	0.0070	0.0080	0.0180
0.5	0.0052	0.0060	0.0066	0.0150
1.0	0.0046	0.0052	0.0051	0.0130
2.0	0.0034	0.0038	0.0045	0.0120
5.0	0.0020	0.0025	0.0043	0.0115
10.0	0.0018	0.0022	0.0042	0.0113
50.0	0.0016	0.0020	0.0040	0.0103

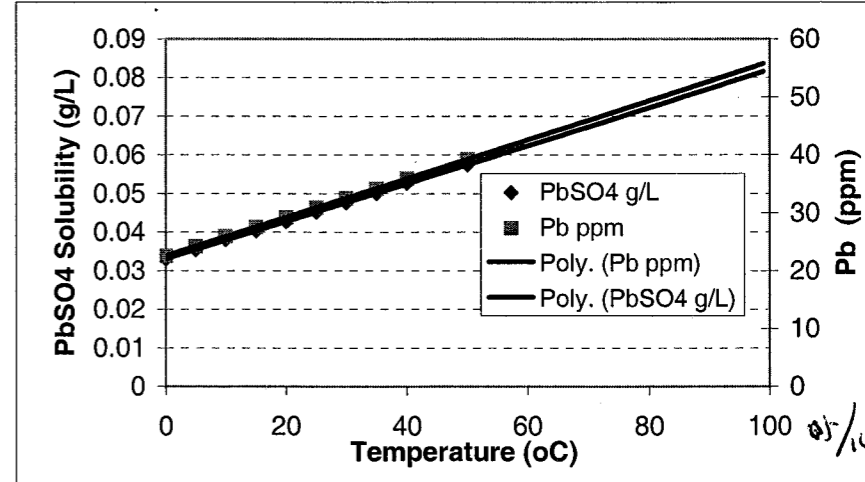
(Cont.)

1320

File: PbSO₄_Solubility

Solubility of PbSO₄ in Water

MW(PbSO ₄)=	303.25
AW(Pb)=	207.2
Temp, oC	PbSO ₄ (g/l) Pb (ppm)
0	0.033 22.54773
5	0.0354 24.18757
10	0.038 25.96406
15	0.0403 27.53556
20	0.0427 29.1754
25	0.0452 30.88356
30	0.0476 32.5234
35	0.05 34.16323
40	0.0526 35.93972
50	0.0574 39.21939
99	



Page 1320, Linke, Solubilities of Inorganic and Metal Organic Compounds -Seidell, Fourth Edition, Volume 2. (1965)
American Chemical Society, Washington, D.C.

Lietai Yang

From:
Sent:
To:
Cc:
Subject:

Lietai Yang [ltyang@gargol.cnwra.swri.edu]
Monday, May 14, 2001 12:01 PM
'ypan@gargol.cnwra.swri.edu'; 'Darrell Dunn (ddunn)'; 'Gustavo Cragnolino'; 'Vijay Jain (vjain)'
'Narasi Sridhar (nsridhar)'
RE: Initial tests for the effect of trace elements



PbSO₄_Solubility.xls

Yi-Ming

Regarding the solubility of PbSO₄ in water, I contacted OLI and realized that they only have the data up to 40oC for PbSO₄(from Seidell). For temperatures greater than 40oC, they assigned a solubility of infinity. This is why we saw no solids at these temperatures. The OLI results at temperatures above 40oC are wrong.

As suggested by Gustavo, I looked at the book, a revision of Seidell's book, and got the solubility data from 0oC to 50oC. The extrapolation to 100oC shows only about 55ppm of Pb solubility (see enclosed file).

I guess you cannot use PbSO₄ in the tests.

Thanks

Lietai

*L. Yang
05/14/01*

*L. Yang
3/10/12*

Lietai Yang

From: Lietai Yang [ltyang@gargol.cnwra.swri.edu]
Sent: Tuesday, May 15, 2001 11:16 AM
To: 'gcragnolino@gargol.cnwra.swri.edu'; 'ypan@gargol.cnwra.swri.edu'; 'Darrell Dunn (ddunn)'; 'Vijay Jain (vjain)'
Cc: 'Narasi Sridhar (nsridhar)'
Subject: RE: Initial tests for the effect of trace elements



Darrell_Pb_Chem_5.xls

Enclosed file shows the amount of NaCl and HCl needed to achieve the same pH and free Cl- concentrations as with the PbCl2 (5000 ppm total Pb) solution. There are two sets of data, one set is to match the pH and Cl- concentration at 25oC and the other set is to match the pH and Cl- at 95oC. The set for 95oC is probably what you want to use.

Yi-Ming, I will do a run to see what is the maximum achievable Pb++ later.

Thanks

Lietai

-----Original Message-----

From: Gustavo Cragnoilino [mailto:gcragnolino@gargol.cnwra.swri.edu]
Sent: Monday, May 14, 2001 3:57 PM
To: ltyang@gargol.cnwra.swri.edu; ypan@gargol.cnwra.swri.edu; 'Darrell Dunn (ddunn)'; 'Gustavo Cragnoilino'; 'Vijay Jain (vjain)'
Cc: 'Narasi Sridhar (nsridhar)'
Subject: RE: Initial tests for the effect of trace elements

It is obvious from Lietai's findings that we should go ahead with PbCl2. Lietai, could you do the calculation to see how much HCl should be added to NaCl to have the same pH that that for PbCl2 as a guide for solution preparation.

J. Yang
8/14/02

From: Yi-Ming Pan [mailto:ypan@gargol.cnwra.swri.edu]
Sent: Friday, May 11, 2001 12:06 PM
To: 'Darrell Dunn (ddunn)'; ltyang@gargol.cnwra.swri.edu; 'Gustavo Cragnoilino'; 'Vijay Jain (vjain)'
Cc: Narasi Sridhar (nsridhar)
Subject: Initial tests for the effect of trace elements

FYI regarding the initial test conditions based on the conclusion of today's meeting, which will include four polarization curve measurements(i.e., two solutions and two materials).

I. Test Solutions

Solution A (from Lietai's calculation)
 Total Pb as PbCl2: 5,000 ppm
 Free Pb++ concentration: 2,400 ppm
 Cl concentration: 0.034 molal
 pH: 3.9
 Temperature: 95C

Solution B

NaCl solution with the same Cl concentration and pH in Solution A

II. Test Materials

Crevice specimens for both alloys 22 and 825

Please let me know if you have any questions and/or comments on the initial test conditions.

Thanks,
 Yiming

Note:

For the free Pb++ concentration, the calculation for Solution A is based on a 5,000 ppm of PbCl2 that was used by Catholic U. The Pb++ concentration depends on the amount of PbCl2 and the resultant Cl concentration. Lietai will perform additional calculations to determine the maximum. In addition, the reference cited in the database for PbSO4 will be evaluated to confirm the almost complete solubility and dissociation of PbSO4 at temperatures above 45C.

J. Yang
8/14/02

Calculation Results requested by Gustavo: 5/15/01

08/17/01

OLI Esp V6.5 / Esp V2.2

Installation test

The following results were obtained with OLI Esp V6.5 / Esp V2.2. The out streams are the outlets of a Mixer Unit. The input was specified such that the outlet streams have Three phases at equilibrium. Therefore the deliquescence point can be calculated using

RH% = (P_h2o / P_h2o^0) * 100 %

Results from ESP V6.2e, May 15, 2001. Pb MW= 207.2 mg (appr. pp mM). Table with columns for PbCl2, NaCl alone, and NaCl + HCl. Rows include Inputs, log(free Cl-), free Pb++ percentage, and Added components like H2O, NaCl, LiCl, HCl, PbCl2, Pb(CH3CO2)2, PbSO4, and Total Pb (ppm).

Stream Phase table with columns for T25oC, T50oC, T95oC for Aqueous, Vapor, and Solid phases. Rows list various chemical species including ACETACID, H2SO4, HCL, SO3, LIOH, NAACET, PBACET2, PBCL2, PBO, LIACET, OHION, CLION, HION, HPBO2ION, HSO4ION, LIOH, LISO4ION, NAION, NASO4ION, ACETATEION, PBACET3ION, PBACETION, PBCL3ION, PBCL4ION, PBCLION, PBIION, PBOHION, SO4ION, PBSO4, NAOL, LIOL, LI2SO4.1H2O, LI2SO4, LIACET.2H2O, LIOL.1H2O, LIOL.2H2O, LIOH.1H2O, NA2SO4.10H2O, NA2SO4, NA3HSO42, NAACET.3H2O, NAHSO4, NAOH.1H2O, NAOH, PBHSO42, PBOH2, Total g/hr, Volume, m3/hr, Enthalpy, cal/hr, Density, g/m3, Vapor fraction, Solid fraction, Organic fraction, Osmotic Pres, atm, Redox Pot, volts, E-Con, 1/ohm-cm, E-Con, cm2/ohm-mol, Abs Visc, cP, Rel Visc, and Ionic Strength.

Property tables for Pure Water, Saturated MgCl2.6H2O, Saturated KCl, and Saturated KNO3. Columns include Phase (Aqueous, Vapor, Solid), Temperature, C, Pressure, atm, pH, Total mol/hr, Flow Units, H2O, HCL, KCL, NANO3, OHION, HION, KION, NO3ION, KNO3, MGION, MGOHION, CLION, MGCL2.6H2O, Total g/hr, Volume, L/hr, Enthalpy, cal/hr, Density, g/L, Vapor fraction, Solid fraction, Organic fraction, Osmotic Pres, atm, Redox Pot, volts, E-Con, 1/ohm-cm, E-Con, cm2/ohm-mol, Abs Visc, cP, Rel Visc, and Ionic Strength.

Relative Humidities at 50oC table with columns for Rel. Hum%, Value, Error, and ASTM Value. Values include 35.10142387, 81.49407678, 88.48945618, 35, 81.2, 84.8, +0.1, +0.3, +2.5.

Continued on page 175 Juyany 8/17/01

Juyany 8/17/01

J.Y. 08/17/01

~~From the table in page 115.~~

The calculated Rel. Humidity (deliquescence point) for the saturated salts are given at the bottom of the table in page 115.

The ASTM values (see page 117) are also given in table of page 115.

The calculated RH values are close to the ASTM values, although it should be noted that for

MgCl₂·6H₂O. The error is $\frac{35.1 - 30.5}{30.5} = 0.15$ which is quite significant. = 15%

J. Yang 08/17/01

E 104 — page 3 (ASTM)

12. Keywords

ANNEXES

(Mandatory Information)

A1. EQUILIBRIUM RELATIVE HUMIDITY VALUES FOR SELECTED SATURATED AQUEOUS SALT SOLUTIONS

Information potentially subject to copyright protection was redacted from this location. The redacted material was extracted from an ASTM manual.

J. Yang 8/17/01

SOFTWARE RELEASE NOTICE

1. SRN Number: CSPE		
2. Project Title: Evolution of Near Field Environment and Container Life Source Term	Project No. 20-01402-561 and 20-01402-571	
3. SRN Title: OLI Software ESP V.6.5 and CSP V2.2		
4. Originator/Requestor: L. Yang	Date: 08/17/01	
5. Summary of Actions		
<input checked="" type="checkbox"/> Release of new software <input type="checkbox"/> Release of modified software: <input type="checkbox"/> Enhancements made <input type="checkbox"/> Corrections made <input type="checkbox"/> Change of access software <input type="checkbox"/> Software Retirement		
6. Persons Authorized Access		
Name	Read Only/Read-Write	Addition/Change/Delete
N. Sridhar	RO	A
L. Yang	RO	A
R. Pabalan	RO	A
V. Jain	RO	A
7. Element Manager Approval:		Date:
8. Remarks: Installation test was performed by L. Yang on 08/17/01 and the results compares with ESP6.2 (scientific Notebook # 430, p.115).		
The comparison with literature data is recorded in Scientific Notebook #430, pages 116 to 117.		

CNWRA Form TOP-6 (05/98)

L.Y. 08/17/01

SOFTWARE SUMMARY FORM

01. Summary Date: 08/17/01	02. Summary prepared by (Name and phone) L. Yang (210)522 2483	03. Summary Action: Updating	
04. Software Date: 03/26/2001	05. Short Title: OLI Software ESP 6.5 and CSP V2.2		
06. Software Title: ESP6.5/CSP2.2			07. Internal Software ID:
08. Software Type: <input type="checkbox"/> Automated Data System <input checked="" type="checkbox"/> Computer Program <input type="checkbox"/> Subroutine/Module	09. Processing Mode: <input checked="" type="checkbox"/> Interactive <input type="checkbox"/> Batch <input type="checkbox"/> Combination	10. Application Area a. General: <input checked="" type="checkbox"/> Scientific/Engineering <input type="checkbox"/> Auxiliary Analyses <input type="checkbox"/> Total System PA <input type="checkbox"/> Subsystem PA <input type="checkbox"/> Other b. Specific:	
11. Submitting Organization and Address: CNWRA/SwRI 6220 Culebra Road San Antonio, TX 78228		12. Technical Contact(s) and Phone: N. Sridhar (210) 522-5538 L. Yang (210) 522-2483	
13. Software Application: This software predicts the speciation of an aqueous solution at given some chemistry conditions. It also predicts metals stability diagrams.			
14. Computer Platform PC	15. Computer Operating System: Windows NT/95/98	16. Programming Language(s): N/A	17. Number of Source Program Statements: N/A
18. Computer Memory Requirements: 40 MB	19. Tape Drives: N/A	20. Disk Units: N/A	21. Graphics: N/A
22. Other Operational Requirements 16 MB RAM required, single user hardware key required			
23. Software Availability: <input type="checkbox"/> Available <input checked="" type="checkbox"/> Limited <input type="checkbox"/> In-House ONLY		24. Documentation Availability: <input checked="" type="checkbox"/> Available <input type="checkbox"/> Preliminary <input type="checkbox"/> In-House ONLY	
25. It is required that OLI systems be paid an annual fee to obtain a "Hardware Key" to allow access each year			
Software User: N. Sridhar and L. Yang		Date: 08/18/01	

CNWRA Form TOP-4-1 (05/98)

L.Y. 08/17/01

Simulation of Evaporation Process for YM Waters

Lietai Yang

From: Roberto Pabalan [rpabalan@gargol.cnwra.swri.edu]
 Sent: Tuesday, September 04, 2001 11:34 AM
 To: Lietai Yang
 Subject: YM water compositions for OLI simulation



YM waters to simulate.doc

Lietai:

See attached file giving the YM water compositions for evaporative simulation using the OLI software.

Thanks.

bobby

software version 6.1.

use total pressure of 0.85 Bar
 and $f_{CO_2} = 1.02E-3$ Bar

— Bobby. 09/04/01

J. Yang
8/14/02

09/10/01

Yucca Mountain water compositions for OLI simulation.

Species	units	UZ-14/1542.3-1542.8	UZ-14/85.2-85.6	NRG-6/158.2-158.6
Ca ²⁺	mg/L	3.6	49.9	122
Mg ²⁺	mg/L	0.5	13.2	23.3
Na ⁺	mg/L	207	43.5	35.6
SiO ₂ (aq)	mg/L	143	89.8	97.4
Al ³⁺	mg/L	13.80	0.30	0.00
HCO ₃ ⁻	mg/L	384	131	34
CO ₃ ²⁻	mg/L	46	0	0
Cl ⁻	mg/L	20	60	185
NO ₃ ⁻	mg/L	4	22	32
SO ₄ ²⁻	mg/L	28	66	159
pH		8.6	6.9	6.8
charge bal.		1.02%	-0.91%	-0.26%
water type		Na-HCO3	Ca-Na-HCO3-Cl-SO4	Ca-Mg-Cl-SO4

Species	units	NRG-6/244.6-245.0	Average J13
Ca ²⁺	mg/L	33	13.00
Mg ²⁺	mg/L	4.9	2.01
Na ⁺	mg/L	72	45.80
K ⁺	mg/L		5.04
SiO ₂ (aq)	mg/L	51	61
Al ³⁺	mg/L	0.60	0
HCO ₃ ⁻	mg/L	61	128.90
CO ₃ ²⁻	mg/L	0	0
Cl ⁻	mg/L	49	7.14
NO ₃ ⁻	mg/L	40	8.78
SO ₄ ²⁻	mg/L	115	18.40
F ⁻	mg/L	na	2.18
pH		7.2	7.41
charge bal.		-2.26%	-0.31%
Water type		Na-Ca-SO4-Cl	Na-Ca-HCO3

Sample Name: UZ-14/1542.3-1542.8 UZ-a
 UZ-14/85.2-85.6 UZ-b
 NRG-6/158.2-158.6 NRG-a
 NRG-6/244.6-245.0 NRG-b
 Average J13 AVG-J13

J. Yang
8/14/02

Chemistry Model

YM_Water

Using Water Analyzer of OLI Tool kit of esp 6.5

With Sample Manager. The samples of 201 inputs were reconciled:

Template Reconcile Units LastResult Help

Sample: UZ-B

YM WATER Study
YM WATER Model
Concentrations

Values in mg/l

Cations	Input	Reconciled	Anions	Input	Reconciled
CA+2	49.9	51.2303	CL-1	60.	59.99975
MG+2	13.2	13.19999	CO3-2		
NA+1	43.5	43.5	HCO3-1	131.	130.9997
AL+3	0.3	0.299999	NO3-1	22.	21.99999
			SO4-2	66.	65.99991

Calc. pH
7.68163

<PgDn>

~~SiO2: 143 mg/L = 0.00238 mol/kg~~ ; added ~ 1 mg/L Ca⁺⁺ for reconciliation

Note: Neutral SiO2 not included here as it is

neutral, it can be included in ESP directly
Jugany zlaboz
SiO2: 89.8 mg/L = 1.495 E-3 mol/kg

Sample UZ-A, Calculated Reconciled pH = 7.31

Template Reconcile Units LastResult Help

YM Water Study
YM WATER Model
Concentrations

Values in mg/l

Cations	Input	Reconciled	Anions	Input	Reconciled
CA+2	3.6	3.599623	CL-1	20.	19.99789
MG+2	0.5	0.4999487	CO3-2	46.	45.99516
NA+1	207.	206.9782	HCO3-1	384.	488.9661
AL+3	13.8	13.79854	NO3-1	4.	3.999582
			SO4-2	28.	27.99708

<PgDn>

not included: SiO2: ~~143 mg/L = 0.00238 mol/kg~~
89.8 mg/L = 1.495 E-3 mol/kg
added HCO3-1 during reconciliation

Sample: NRE-A, Calculated pH = 7.93

Template Reconcile Units LastResult Help

YM WATER Study
YM WATER Model
Concentrations

Values in mg/l

Cations	Input	Reconciled	Anions	Input	Reconciled
CA+2	122.	122.959	CL-1	185.	184.9998
MG+2	23.3	23.29997	CO3-2		
NA+1	35.6	35.59985	HCO3-1	34.	33.99998
AL+3			NO3-1	32.	31.99995
			SO4-2	159.	158.9996

1.6218 mol/l

Jugany zlaboz

Not included: SiO2: 97.4 mg/L, added Ca²⁺

Sample NRG-B

Calculate pH Reconcile pH Help

YM_WATER Study
YM_WATER Model
Sample NRG_B

Sample NRG_B

Measured pH: 0.0

Calculated pH: 7.4225

YM_WATER Study
YM_WATER Model
Concentrations

Values in mg/l

Cations	Input	Reconciled	Anions	Input	Reconciled
CA+2	33.	32.99988	CL-1	49.	48.99978
MG+2	4.9	4.899972	CO3-2		
NA+1	72.	75.96943	HCO3-1	61.	60.99961
AL+3	0.6	0.5999973	NO3-1	40.	39.99986
			SO4-2	115.	114.9992

Not included: $SiO_2 = 0.749E-3 \text{ mol/kg}$ added that to reconcile: 51 mg/L

Sample AVG-J13, Calculated pH: 8.07

YM_WATER Study
YM_WATER Model
Concentrations

Values in mg/l

Cations	Input	Reconciled	Anions	Input	Reconciled
AL+3			CL-1	7.14	7.139547
CA+2	13.	12.9992	CO3-2		
K+1	45.8 5.04	45.79733	F-1	2.18	2.179869
MG+2	2.01	2.009874	HCO3-1	128.9	191.3923
NA+1	45.8	45.79708	NO3-1	8.78	8.779436
			SO4-2	18.4	18.39888

Not included: $SiO_2 = 61 \text{ mg/L}$; $60 \text{ mg } HCO_3-1$ was added

mg/L
13/10/1
mg
Page 132

The above files are converted into OLI stream files using OLI Stream Manager under: OLI Toolkit.

new OLI stream files.

original files

Utility Send Help

YM_WATER Study
YM_WATER Model
Sample AVG_J13

WORKING WITH WHICH ESP STREAM?

New OLI Stream	Based On:	Sent To:
AVG_J13	AVG_J13	
NRG_B	NRG_B	
NRG_A	NRG_A	
UZ_B	UZ_B	
UZ_A	UZ_A	

Successfully created OLI Stream AVG_J13
<Esc> Quit <F1> Help <F3> End (Save) <F10> Actions <Enter> Continue

Jayan 8/10/02

Back to Esp. created a new process

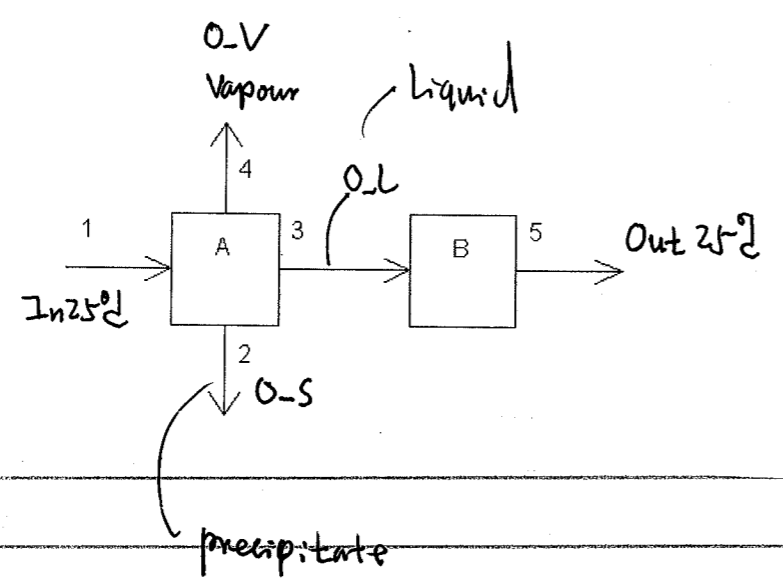
YM_water - process Name

YM_water process Jy. 09/26/01

Process Build:

Scroll up | Scroll down | Exit

1. In2502
2. O-V
3. O-L
4. O-S
5. O-L
6. S
7. P
8. P
9. P
10. P
11. P
12. P
13. P
14. P
15. P
16. P
17. P
18. P
19. P
20. P
21. P
22. P
23. P
24. P
25. P
26. P
27. P
28. P
29. P
30. P
31. P
32. P
33. P
34. P
35. P
36. P
37. P
38. P
39. P
40. P
41. P
42. P
43. P
44. P
45. P
46. P
47. P
48. P
49. P
50. P
51. P
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81. P
82. P
83. P
84. P
85. P
86. P
87. P
88. P
89. P
90. P
91. P
92. P
93. P
94. P
95. P
96. P
97. P
98. P
99. P
100. P



A - a separator,
B - a mixer.

A - set to isothermal at constant P = 0.27 atm. Jy. 10/23/01

B - set to isothermal at const. 25°C.

Stream Out 2502 is the composition for liquid sampled at the O-L stream condition (T and P). Jy. 10/23/01

Load the ^{OLI} stream files in Page 125 for In2502.
" * .Smp "

OLI Stream UZ_A

ALOH3	0.511914E-03			
CAOH2	0.899044E-04			
H2CO3	0.864287E-02			
HCL	0.564627E-03			
HNO3	0.645682E-04			
MGOH2	0.205902E-04			
NA6SO42CO3	0.145866E-03			
NAOH	0.813669E-02			
SCALE ALOH3PPT	0.100000D+01	273.150	373.150	
SCALE ALOOHPPPT	0.738618D+00	373.250	523.150	EXCL TR
SCALE NAALCO3OH2PPT	0.121568D+00			
SCALE CACO3PPT	0.114807D+00			

SiO2 to add: 2.38 E-3 mol/kg.
H2O H2O3 mol

OLI Stream UZ_B

ALOH3	0.111237E-04			
CAOH2	0.127884E-02			
H2CO3	0.186058E-02			
HCL	0.169314E-02			
HNO3	0.354971E-03			
MGOH2	0.543344E-03			
NA3HSO42	0.563604E-04			
NA6SO42CO3	0.287317E-03			
SCALE ALOH3PPT	0.100000D+01	273.150	373.150	
SCALE CACO3PPT	0.100000D+01			
SCALE ALOOHPPPT	0.738477D+00	373.250	523.150	EXCL TR
SCALE CASO4.2H2O	0.130814D-01	273.150	373.150	

SiO2: 1.45E-3 mol/kg. Jy. 10/23/01

YM WATER Study YM WATER Model OLI Stream NRG_A				
CAOH2	0.307026E-02			
H2CO3	0.557630E-03			
H2SO4	0.623280E-03			
HCL	0.522202E-02			
HNO3	0.516468E-03			
MGOH2	0.959356E-03			
NA3HSO42	0.516545E-03			
SCALE CACO3PPT	0.969737D+00			
SCALE CASO4.2H2O	0.565979D-01	273.150	373.150	
SCALE CASO4PPT	0.405024D-01	373.150	523.150	EXCL TR
END				

1.621 E-3 mol/kg SiO2

YM WATER Study YM WATER Model OLI Stream NRG_B				
ALOH3	0.222466E-04			
CAOH2	0.823735E-03			
H2CO3	0.496991E-03			
HCL	0.138268E-02			
HNO3	0.645378E-03			
MGOH2	0.201688E-03			
NA3HSO42	0.956701E-04			
NA6SO42CO3	0.503138E-03			
SCALE ALOH3PPT	0.100000D+01	273.150	373.150	
SCALE ALOHPPT	0.738476D+00	373.250	523.150	EXCL TR
SCALE CACO3PPT	0.167579D+00			
SCALE CASO4.2H2O	0.154617D-01	273.150	373.150	

0.849 E-3 mol/kg SiO2

adjust slurb

YM WATER Study YM WATER Model OLI Stream AVG_J13	
CAOH2	0.324475E-03
H2CO3	0.304212E-02
HGF6	0.191308E-04
HNO3	0.141648E-03
KMGCL3	0.671532E-04
KOH	0.110464E-02
MGOH2	0.155731E-04
NA6SO42CO3	0.958015E-04
NAOH	0.141802E-02
SCALE CACO3PPT	0.100000D+01
SCALE CAF2PPT	0.104042D+00
END	

SiO2: 1.01E-3 mol/kg

Re adjust the chemistry model to include SiO2 and every chemical species in the above 5 waters.

→ YM-water (still call it this name)

The revised file on page 124 has an error. this table is redone. see page 132

J. Yang
slurb

Verification of the reconciled stream:

File: YM_Water_Recociliation_Verification.xls

From Page 121

U2-A

Species	FW	mg/L					mol/L				
		UZ-14/1542.3-1542.8	UZ-14/85.2-85.6	NRG-6/158.2-158.6	NRG-6/244.6-245.0	Average J13	UZ-14/1542.3-1542.8	UZ-14/85.2-85.6	NRG-6/158.2-158.6	NRG-6/244.6-245.0	Average J13
		UZ_A	UZ_B	NRG_A	NRG_B	AVG_J13	UZ_A	UZ_B	NRG_A	NRG_B	AVG_J13
Ca2+	40	3.6	49.9	122	33	13	9.00E-05	1.25E-03	3.05E-03	8.25E-04	3.25E-04
Mg2+	24.3	0.5	13.2	23.3	4.9	2.01	2.06E-05	5.43E-04	9.59E-04	2.02E-04	8.27E-05
Na+	23	207	43.5	35.6	72	45.8	9.00E-03	1.89E-03	1.55E-03	3.13E-03	1.99E-03
K+	39.1					5.04					1.29E-04
SiO2(aq)	60.09	143	89.8	97.4	51	61	2.38E-03	1.49E-03	1.62E-03	8.49E-04	1.02E-03
Al3+	27	13.8	0.3	0	0.6	0	5.11E-04	1.11E-05	0.00E+00	2.22E-05	0.00E+00
HCO3-	61	384	131	34	61	128.9	6.30E-03	2.15E-03	5.57E-04	1.00E-03	2.11E-03
CO32-	60	46					7.67E-04				
Total CO32-							7.06E-03	2.15E-03	5.57E-04	1.00E-03	2.11E-03
Cl-	35.5	20	60	185	49	7.14	5.63E-04	1.69E-03	5.21E-03	1.38E-03	2.01E-04
NO3-	62	4	22	32	40	8.78	6.45E-05	3.55E-04	5.16E-04	6.45E-04	1.42E-04
SO42-	96	28	66	159	115	18.4	2.92E-04	6.88E-04	1.66E-03	1.20E-03	1.92E-04
F-	19			na		2.18					1.15E-04
pH		8.6	6.9	6.8	7.2	7.41					
charge bal.		1.02%	-0.91%	-0.26%	-2.26%	-0.31%					
water type		Na-HCO3	Ca-Na-HCO3-Cl-SO4	Ca-Mg-Cl-SO4	Na-Ca-SO4-Cl	Na-Ca-HCO3	Na-HCO3	Ca-Na-HCO3-Cl-SO4	Ca-Mg-Cl-SO4	Na-Ca-SO4-Cl	Na-Ca-HCO3

Recociled Compounds: from page 127

U2-A

AlOH3	5.12E-04
CaOH2	8.99E-05
H2CO3	8.64E-03
H6F6	
H2SO4	
HCl	
HNO3	5.65E-04
KMgCl3	6.46E-05
KOH	
MgOH2	
Na3HSO42	2.06E-05
Na6SO42CO3	
NaOH	1.46E-04
	8.14E-03

compared well.

Aug. 9/13/01

ions from Reconciled compound above

Ca2+	8.99E-05
Mg2+	2.06E-05
Na+	9.01E-03
K+	0.00E+00
SiO2(aq)	
Al3+	
HCO3-	5.12E-04
CO32-	
Total CO32-	8.79E-03
Cl-	5.65E-04
NO3-	6.46E-05
SO42-	2.92E-04
F-	0
added by mol/L	HCO3- 1.72E-03
by mg/L	104.97

$(8.79 - 1.72) \times 10^{-3} = 7.07 \times 10^{-3}$

The reconciled file included the added 104.97 mg/L of HCO3-

(see page 123)

Jugur Alimbar

Concentration factor

J.G. 09/20/01

In DOEJ Report. Page 15, ^{cont page 13} AML-EBS-MD-0004-REV (April 2000)

The concentration factor is the ratio of the initial water mass divided by the water mass at the time of analysis.

My understanding is not to include the solutes in the water, not solid either!

J. Yang 09/18/01

09/17/01

Found an error for AVG-J13 reconciled result. (page.124) k+ should be 5.04 mg/L

newly reconciled results are given in page 132

J. Yang

8/10/02

Recalculation of AVG-J13 (from pages 124 and 129.)

YM WATER Study
YM WATER Model
Concentrations

Values in mg/l

Cations	Input	Reconciled	Anions	Input	Reconciled
AL+3			OH-1		
CA+2	13.	13.00001	CL-1	7.14	7.139998
H+1			CO3-2		
K+1	5.04	5.040011	F-1	2.18	2.179998
MG+2	2.01	2.01	H3SIO4-1		
NA+1	45.8	46.21689	HCO3-1	128.9	128.9002
			HSO4-1		
			NO3-1	8.78	8.779968
			SO4-2	18.4	18.39999

<PgDn>

PH = 7.186
 SiO2: 61 mg/l not included. = 1.01E-3 mol
 NaCl: 24 mg/l added for recalculation

After converted into OLI Stream Files:

YM WATER Study
YM WATER Model
OLI Stream AVG_J13

OLI Stream AVG_J13

CAOH2	0.324456E-03
H2CO3	0.201730E-02
H6F6	0.191296E-04
HNO3	0.141640E-03
KMGCL3	0.671493E-04
KOH	0.617918E-04
MGOH2	0.155721E-04
NA6SO42CO3	0.957958E-04
NAOH	0.143607E-02
SCALE CACO3PPT	0.999470D+00
SCALE CAF2PPT	0.117995D+00
END	

<PgUp>

tho: 55.509 mol/hr
 J. J. 8/14/02

Summary of Modeling Results with OLI ESP 6.5
 9/21/2001
 File: YM_Water_Total_Ionic.xls

Sheet Contents
 This workbook contains the following worksheets:
 Original_Data: Data from OLI (Zero rows deleted, the number column shows the original row number)
 Stream_O_L: Data for Syream O_L
 Stream_O_L_Ignored_Zero_Rows: Data for Syream O_L after deleted the zero rows for the O_L stream
 Chart_Stream_O_L: Chart according to data on Stream_O_L_Ignored_Zero_Rows
 Stream_O_L_Ions_Only: Data for Syream O_L after deleted non ionic rows
 Chart_Stream_O_L_Ions: Chart according to data on Stream_O_L_Ions_Only

Flowsheet used in Modelling:

* Feed:
 UZ_A: UZ-14/1542.3-1542.8
 UZ_B: UZ-14/85.2-85.6
 NRG_A: NRG-8/158.2-158.6
 NRG_B: NRG-8/244.6-245.0
 AVG_J13: Average J13

Notations of Selected Labels:
 Water: Feed Name
 Variable T, oC: Temperature
 Variable Con of added CO2 to Feed (mola): CO2 added to the feed to adjust the P(CO2) in the O_L stream
 Pressure, atm: Pressure, atm
 Conc. Factor (Derived): Concentration factor: Ratio of Water in O_V to Water in O_L **
 P of Pure H2O at T: Vapour Pressure of H2O at T
 R Humidity at T: Relative Humidity in the Separator or Streams D_H of O_L
 P(CO2, atm): Fugacity of CO2 in Separator
 Ionic Strg.* (Software Maximum, 30)
 X(H2O) (Software Minimum, 0.65): Mole Fraction of water in O_L stream

For Molecular Phase output Results, please see the following five Spreadsheet Files:
 YM_Water_UZ_A.xls
 YM_Water_UZ_B.xls
 YM_Water_NRG_A.xls
 YM_Water_NRG_B.xls
 YM_Water_AVG_J13.xls

* Flow sheet shown in page 126 was abandoned.
 J.J. 09/21/01
 Example outputs

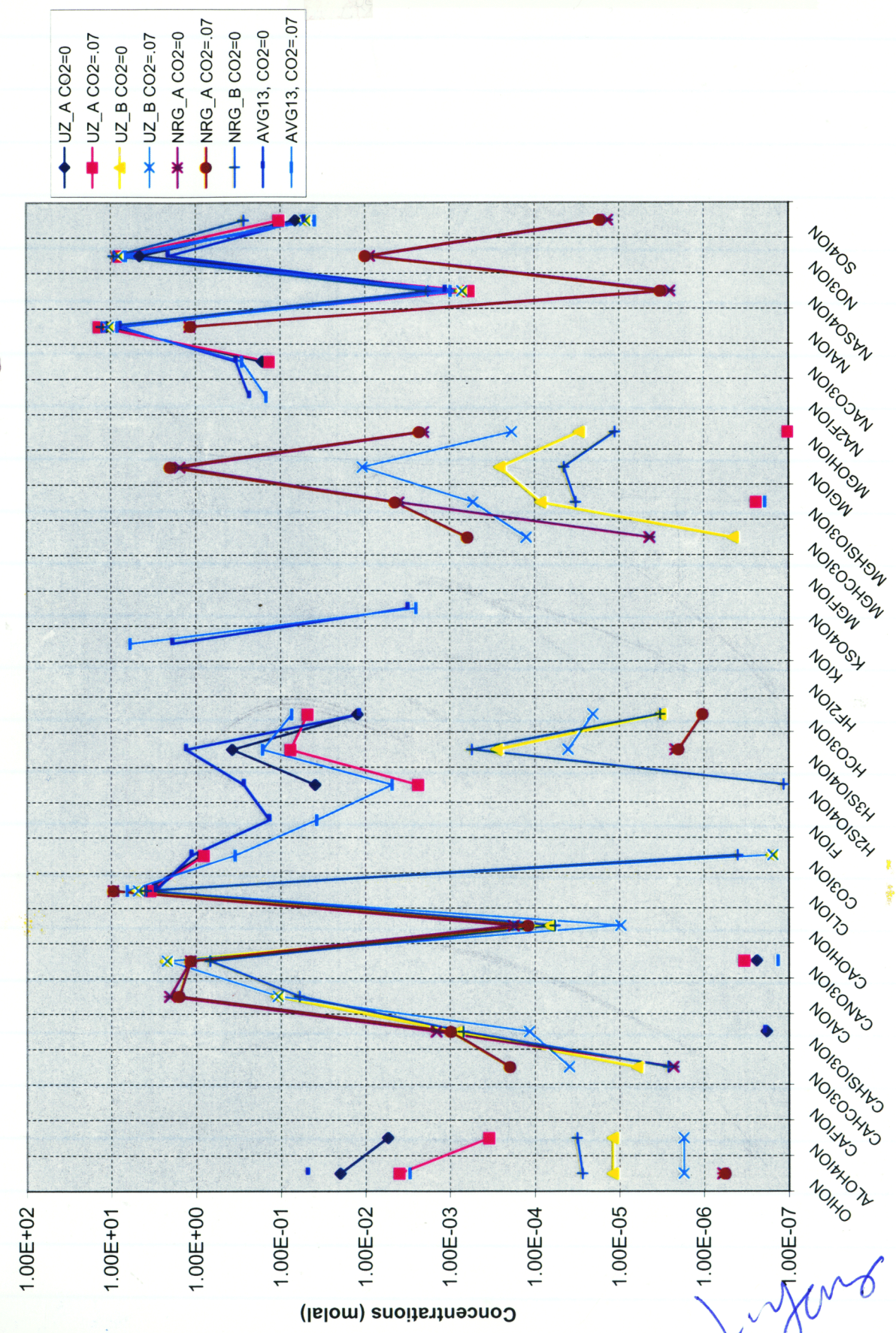
Definition see page 131

J. J.
 8/14/02

Stream	UZ_A	UZ_A	O.V	O.L
Phase	Aqueous	Solid	Vapor	Aqueous
Temperature, C	25	25	110	110
Pressure, atm	1	1	0.85	0.85
pH	7.33586			10.6325
Total mol/hr	55.53845	9.76E-04	55.5265	8.17E-05
Flow Units	mol/hr	mol/hr	mol/hr	mol/hr
1 H2O	55.5178		55.52198	5.56E-05
2 H2F2				
3 CO2	7.33E-04		0.00451583	1.12E-13
4 H2SO4	1.49E-27			
5 HCL	1.39E-17		5.25E-12	1.38E-21
6 HF				
7 HNO3	9.41E-15		4.69E-12	8.33E-18
9 SIF4				
10 SO3				
11 CASO4	1.34E-06			3.89E-17
12 ALOH3	2.40E-09	5.12E-04		2.56E-15
13 KCL				
14 KHCO4				
15 MGCO3	7.95E-08			6.25E-14
16 MGH2SIO4	6.21E-11			3.09E-13
17 MGSO4	1.42E-07			3.30E-18
18 NAF				
19 NAHCO3	2.45E-05			2.44E-08
20 NAHSIO3	5.82E-06			4.69E-06
21 NANO3	6.14E-10			4.23E-08
23 CACO3	8.56E-07			8.75E-13
24 SIO2	0.0019037	4.64E-04		1.90E-09
25 CAH2SIO4	3.12E-11			1.37E-13
26 OHION	2.43E-07			2.00E-06
31 ALION	2.40E-15			
32 ALOH2ION	2.25E-11			1.93E-21
33 ALOH4ION	1.45E-08			5.49E-09
34 ALOHION	3.09E-13			1.21E-28
35 ALSO42ION	3.02E-18			
36 ALSO4ION	2.03E-16			
37 CAFION				
38 CAHCO3ION	4.92E-06			4.09E-15
39 CAHSIO3ION	6.59E-09			1.84E-13
40 CAION	8.28E-05			2.25E-14
41 CANO3ION	6.62E-10			2.43E-13
42 CAOION	2.28E-10			2.22E-14
43 CLION	5.65E-04			4.18E-06
44 CO3ION	1.11E-05			8.21E-07
45 FION				
46 H2SIO4ION	1.53E-11			3.92E-08
47 H3SIO4ION	6.57E-06			3.75E-07
48 HCO3ION	0.0080102			1.24E-08
49 HF2ION				
50 HION	5.10E-08			9.90E-18
51 HSO4ION	9.21E-10			1.17E-18
52 KION				
53 KSO4ION				
54 MGFION				
55 MGHCO3ION	3.43E-06			4.89E-16
56 MGHHSIO3ION	2.50E-09			5.30E-14
57 MGION	1.89E-05			5.80E-16
58 MGOHION	4.50E-10			2.84E-14
59 NA2FION				
60 NACO3ION	2.33E-07			1.64E-07
61 NAIION	0.0089796			1.11E-05
62 NASO4ION	1.78E-08			6.43E-10
63 NO3ION	4.57E-06			4.53E-06
65 SIF6ION				
66 SO4ION	2.88E-04			6.64E-08
74 NA6SO42CO3				
75 MGOH2				
84 ALOOH				
95 CASO4.2H2O				
108 KNO3				
117 MGF2				
129 NA2CO3				
131 NA2SO4				
133 NAALCO3OH2				
136 NACL				
181 Totalg/hr	1001.07	0.0678034	1000.45	0.00227164
182 Volume, L/hr	1.00359	2.90E-05	2040.29	1.47E-06
183 Enthalpy, cal/hr	-3.80E+06	-2.58E+02	-3.17E+06	-6.64E+00
184 Density, g/L	997.49	2337.16	0.490345	1550.28
185 Vaporfraction			1	
186 Solidfraction				1
187 Organicfraction				
188 OsmoticPres, atm	0.479577			877.248
189 RedoxPot, volts				
190 E-Con, 1/ohm-cm	8.37E-04			0.6401
191 E-Con, cm2/ohm	40.9822			0.043295
192 AbsVisc, cP	0.894802			1.61256
193 RelVisc	1.00458			6.3342

File: ym_water_Total_Ionic.xls / Tab: Chart_Stream_O_L_ions

in note book directory



Handwritten notes: "J. Yang" and "8/14/02" written vertically.

Handwritten conditions: $T = 110^{\circ}C$ and $P = 0.85 \text{ atm}$.

File: ym_water_EVap.xls / Tab: Ym_water_total_ionic

Source:

This Sheet is copied from the sheet with Zero Rows Deleted in File: ym_water_Total_Ionic.xls

CO2 in Feed (molal)	0	0.07	0	0.07	NRG_A	NRG_A	NRG_B	AVG_J13	AVG_J13
Molals (C>1e-7)	UZ_A	UZ_A	UZ_B	UZ_B	0	0.07	0	0	0.07
3 CO2	1.12E-07	1.3E-06		2.6E-06			4.18E-06		
7 HNO3				2.17E-07					2.84E-06
11 CASO4			0.000325	0.000324	0.000155	0.00015	0.000289		
13 KCL									
15 MGCO3		9.54E-07		1.28E-06				0.028511	0.086039
16 MGH2SIO4	3.09E-07	2.86E-07	4E-07	4E-07	1.91E-07	1.85E-07	3.56E-07	3.9E-07	3.02E-07
17 MGSO4			9.98E-06	0.000437	0.000124	0.000199	3.99E-06		
18 NAF									
19 NAHCO3	0.024407	0.091638	7.23E-06	4.78E-05				0.113455	0.044046
20 NAHSIO3	4.682643	1.066844	0.003832	0.000579	6.27E-06	5.32E-06	7.39E-06	0.018008	0.094567
21 NANO3	0.042275	0.071294	0.110955	0.111682	2.12E-05	2.66E-05	0.099309	10.10267	1.153555
23 CACO3	8.74E-07	8.09E-07	1.13E-06	1.13E-06				0.014468	0.031341
24 SIO2	0.001901	0.00169	0.002552	0.002545	0.001621	0.001567	0.002289	1.1E-06	8.55E-07
25 CAH2SIO4	1.37E-07		4.89E-07					0.0022	0.00214
26 OHION	0.01998	0.003928	1.17E-05	1.77E-06	5.99E-07	5.57E-07	9.65E-07	5.04E-07	
33 ALOH4ION	0.00549	0.000345	1.17E-05	1.78E-06			2.8E-05	0.048496	0.003034
38 CAHCO3ION			6.02E-06	3.98E-05	2.28E-06	0.000194	2.7E-06		
39 CAHSIO3ION	1.84E-07		0.000781	0.000118	0.001439	0.000967	0.000704	1.94E-07	
40 CAION			0.107076	0.107546	2.008151	1.550909	0.060095		
41 CANO3ION	2.43E-07	3.32E-07	2.184817	2.180375	1.142855	1.133872	0.686056		1.37E-07
42 CAOHION			6.53E-05	9.81E-06	0.000176	0.000119	5.83E-05		
43 CLION	4.174277	3.398285	4.791008	4.768404	9.332072	9.247634	3.850956	2.951193	6.417751
44 CO3ION	0.820127	0.802104	1.55E-07	1.57E-07			4.07E-07	1.130449	0.344798
45 FION								0.135464	0.037656
46 H2SIO4ION	0.039129	0.002319						0.271092	0.004832
47 H3SIO4ION	0.375021	0.075066	0.000272	4.1E-05	2.16E-06	1.96E-06	0.000559	1.30611	0.163199
48 HCO3ION	0.012392	0.046864	3.14E-06	2.08E-05		1.02E-06	3.34E-06	0.011915	0.074018
50 HION					7.07E-07	7.96E-07			
52 KION									
53 KSO4ION								1.875587	5.909292
55 MGHCO3ION			4.38E-07	0.000127	4.33E-06	0.000609		0.003127	0.002515
56 MGHSIO3ION		2.38E-07	8.13E-05	0.000537	0.003906	0.004337	3.3E-05		1.93E-07
57 MGION			0.000248	0.010787	1.512397	1.945774	4.52E-05		
58 MGOHION			2.85E-05	0.000188	0.001997	0.002232	1.14E-05		
59 NA2FION									
60 NACO3ION	0.16341	0.133033						0.230504	0.146505
61 NAION	11.12424	13.5169	10.44812	10.45521	1.149296	1.121734	12.71917	0.332792	0.282526
62 NASO4ION	0.000643	0.00058	0.000711	0.000715	2.47E-06	3.21E-06	0.001804	0.001125	0.000979
63 NO3ION	4.52175	8.046178	7.956995	8.004133	0.008664	0.009744	9.135558	2.080597	6.557243
66 SO4ION	0.06638	0.101892	0.049773	0.049974	1.34E-05	1.66E-05	0.268687	0.052131	0.038773

Handwritten note: "Pcon (From data file) (atm)"

Handwritten values: $2.36E-5, 1.09E-3$

Handwritten signature: "J. Yang" and "8/14/02"

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and given to QA for record

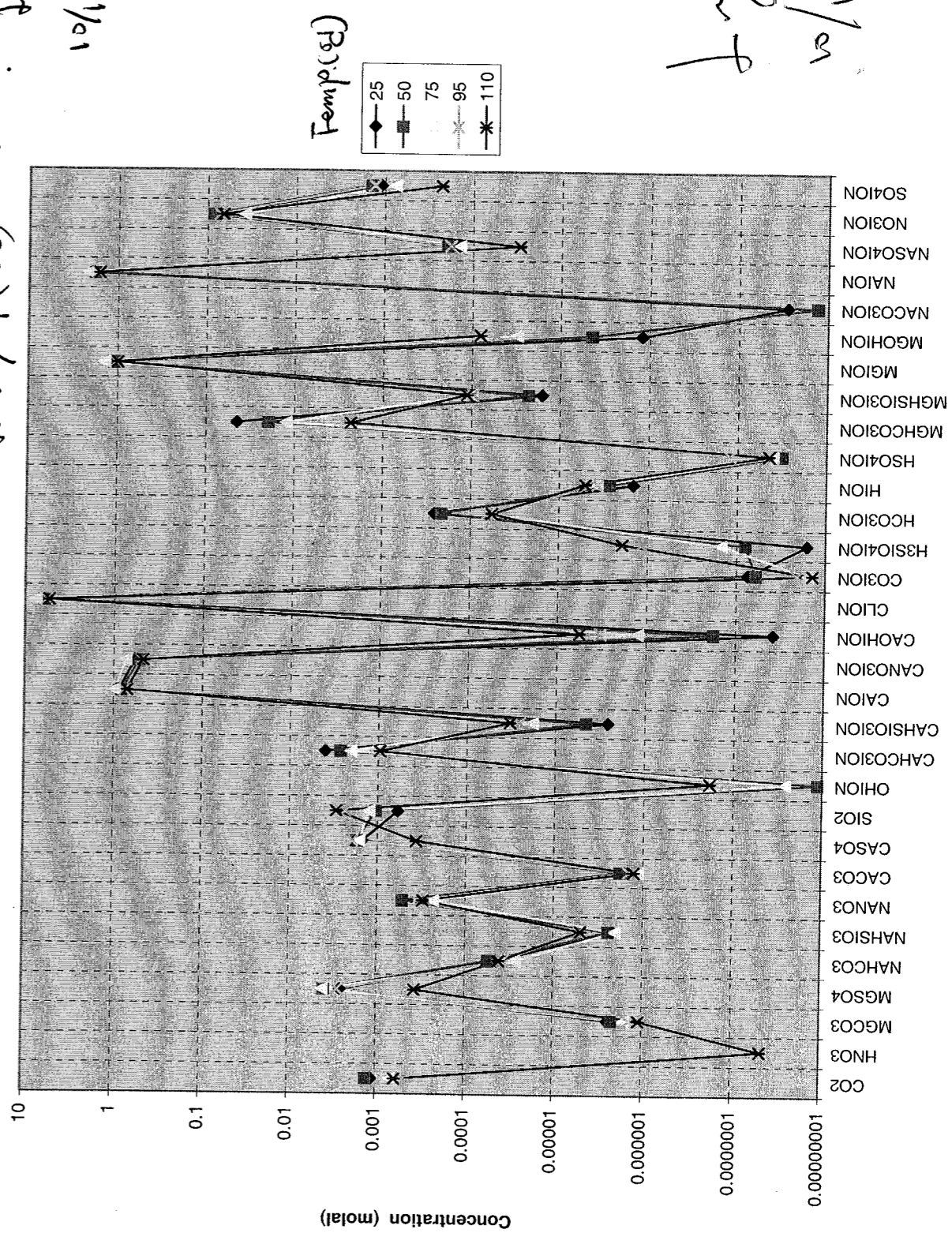
J. Young

10/05/01

File: ym_NRG_A_VaryingT_f=1200_PCO2=1E-1.xls Tab: Chart_Based_On_O_L_ZeroRowsDel

f - concentration factor / P(CO2) = 0.1 atm.

12/01/01
J. Young



12/01/01
J. Young

