



International Agreement Report

Assessment of RELAP5/MOD2 Against ECN-Reflood Experiments

Prepared by
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**Office of Nuclear Regulatory Research
U.S. Nuclear Regulatory Commission
Washington, DC 20555-0001**

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Prepared as part of
The Agreement on Research Participation and Technical Exchange
under the International Thermal-Hydraulic Code Assessment
and Application Program (ICAP)

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ABSTRACT

As part of the ICAP (International Code Assessment and Applications Program) agreement between ECN (Netherlands Energy Research Foundation) and USNRC, ECN has performed a number of assessment calculations with the computer program RELAP5.

This report describes the results as obtained by ECN from the assessment of the thermohydraulic computer program RELAP5/MOD2/CY 36.05 versus a series of reflood experiments in a bundle geometry. A total number of seven selected experiments have been analyzed, from the reflood experimental program as previously conducted by ECN under contract of the Commission of the European Communities (CEC). In this document, the results of the analyses are presented and a comparison with the experimental data is provided.

EXECUTIVE SUMMARY

For both Pressurized and Boiling Water Reactors (PWR's and BWR's) the bottom reflooding process following a large break LOCA is one of the phenomena of great interest to be examined. To test the ability of RELAP5/MOD2 to model such conditions a great number of experimental programs has been conducted to study the reflood heat transfer process and quench front propagation for bottom flooding conditions. The assessment calculations as reported in this document concern reflood experiments as conducted by the Netherlands Energy Research Foundation (ECN). The experimental facility represents a 36-rod bundle segment of a standard 15 x 15 PWR fuel design with an axially uniform power profile.

This report describes comparisons between RELAP5/MOD2 calculations and measurements of wall temperatures at different levels, quench front position, collapsed liquid level, mass inventory in the bundle and integrated boundary mass flows.

The prime conclusions are as follows:

- The RELAP5/MOD2 reflood heat transfer model is only valid for high reflood rates.
- Liquid carry-over is strongly overpredicted.
- Refinement of axial nodalization above the recommended value did not improve the calculational results.

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1. INTRODUCTION

As part of the International Code Assessment and Applications Program (ICAP) agreement between the Netherlands Energy Research Foundation (ECN) and the United States Nuclear Regulatory Commission (US-NRC), ECN has conducted a number of assessment calculations using the thermohydraulic system code RELAP5/MOD2/CY 36.05. ref. [1]. The assessment calculations as reported in this document concern a selection of seven reflood experiments as conducted by ECN under contract of the Commission of the European Communities (CEC). The results of this ECN-reflood experimental program have been documented in ref. [2].

As described in NUREG-1271, ref. [5], quantification of code uncertainty for Large Break Loss-of-Coolant Accidents (LB-LOCA), Small Break Loss-of-Coolant Accidents (SB-LOCA) and operational transients requires a large number of assessment calculations to be performed for a variety of integral as well as separate effect experiments. For each of these three classes of accidents, phenomenologically based code assessment matrices have been composed for both the Pressurized and Boiling Water Reactors environment (PWR's and BWR's). One of the phenomena to be examined concerns the reflooding process following LB-LOCA in both PWR's and BWR's. A number of separate effect experimental programs have been conducted to study the reflood heat transfer process and quench front propagation for bottom flooding conditions. Table 1.1 lists some of these experimental programs including their main characteristics. As can be observed from this table, the ECN-reflood experimental facility represents a 36-rod bundle segment of a standard 15 x 15 PWR fuel design. The ECN-reflood experimental program differs from other reflood experimental programs by the axially uniform power profile being used.

RELAP5/MOD2 reflood assessment results already available indicate that discrepancies exist between code predictions and experimental results, ref. [3]. Liquid carry-over is grossly overpredicted and therewith underprediction of the collapsed liquid level occurs. Most of this RELAP5/MOD2 assessment work indicates the cause of overprediction of carry-over is an overestimation of the interphase drag in rod bundle geometries, particu-

larly in the slug flow regime. As stated in ref. [3], most of the RELAP5/MOD2 interphase drag model assessment during the development stage has been based mainly on tube and open vessel data, and only to a minor extent on rod bundle data.

The ECN-reflood data base comprises a total of 48 experiments. Out of this data base, a total of seven experiments have been selected for code assessment, based on the different physical phenomena observed during the experiments and the parameter variations used.

The structure and contents of this assessment document is as much as possible in conformity with the guidelines described in NUREG-1271, ref. [5]. Chapter 2 presents a description of the ECN-reflood experimental facility, the operating procedures and the test matrix. In chapter 3 the RELAP5/MOD2 input model is being described, as well as the initial and operating conditions of the selected experiments. The results of the RELAP5/MOD2 analyses are presented in chapter 4 and compared against the experimental data. Sensitivity analyses with respect to e.g. nodalization are also given in chapter [4]. Information with respect to run statistics can be found in chapter 5, followed by the conclusions in chapter 6. Finally, the RELAP5/MOD2 input deck being used for one of the experiments is being shown in Appendix A.

Table 1.1. Comparison of some reflood experimental facilities.

	No. of rods	Height (%)	Axial power profile	Remark
Flecht	7 x 7 & 10 x 10	100	Cosine, Skewed	15 x 15
Flecht seaset	21, 161, 163	100	Cosine, Skewed	17 x 17
Neptun	6 x 6	50	Cosine	BWR geometry
THTF	8 x 8	100	Flat	PWR 17 x 17 rod geometry
ECN-reflood	6 x 6	100	Uniform	PWR 15 x 15 rod geometry

2. FACILITY AND TEST DESCRIPTION

An extensive description of the ECN 36-rod reflood experimental program can be found in ref. [2]. Here, only a brief description of the facility and the experimental program will be given.

2.1. Geometrical layout

A schematic picture of the ECN 36-rod reflood test facility is shown in Fig. 2.1. Apart from the test section, the facility consists of the following components:

- A pressurized water supply accumulator and injection line;
- Two carry-over tanks connected to the test section upper plenum;
- A blowdown tank for steam condensation.

Heat tracing of piping and vessels has been utilized to prevent steam condensation effects.

The test section itself comprises a 36-rod bundle, located inside a rectangular low mass housing. The bundle consists of 32 electrically heated rods and 4 unheated corner rods, which are used to bear instrumentation, instrumentation leads and the grids. The indirectly heated rods (heated length 3.00 m, outer diameter 10.7 mm) are divided into three concentric rows. Axially a uniform power profile is applied, while radially the 4 centre rods, the inner row and the outer row heater rods can be set at different power levels to establish a radially non-uniform power or initial wall temperature profile. The upper plenum of the test section contains a mechanical steam water separator, see Fig. 2.2.

2.2. Instrumentation

The ECN 36-rod reflood test facility has been instrumented using:

- thermocouples for temperature measurements;
- flowmeters for steam and water flow measurements;
- pressure transducers for absolute pressures, pressure differences and water level measurements;
- resistors for heater current measurements.

The overall test facility instrumentation is shown in Fig. 2.1. Instrumentation directly coupled to the test section is shown in Figs. 2.3 and 2.4. As indicated, housing differential pressure cells are located every 0.25 m to obtain void fraction measurements along the heated length of the bundle. Channel thermocouples are mounted to measure the coolant temperature radially and axially across the bundle. Apart from this, wall thermocouples are positioned at 8 levels per rod at different azimuthal positions, as shown in Fig. 2.4.

2.3. Operational procedures

In order to meet the initial conditions for each experiment, first the accumulator is filled with water and heated to the desired coolant temperature. Next, the test section, the carry-over vessels and steam/water separator vessel are pressurized by nitrogen at the desired pressure. The accumulator is pressurized with nitrogen up to a pressure level which is necessary for the required flow rate control.

In case of radially uniform initial temperature profiles, the bundle was initially low powered. For radially non-uniform high temperature profiles, a radially non-uniform power profile was initially supplied to the bundle.

Once the initial pressure and temperature conditions are met, the desired coolant flow is established. At the time when the coolant reached the bottom side of the test section heated length the power is (stepwise) increased to the desired level. This moment is determined by a fast temperature increase of the heater rod thermocouple at level 1, see Fig. 2.3. This time, which could also be determined by a pressure increase of the lowest differential pressure cell in the heated part of the test section is defined as the "start of the experiment".

After all heater rods are quenched, as could be observed from the rod wall thermocouple measurements, the heater power is switched off, and the experiment is terminated.

2.4. Test matrix

The test matrix of the experimental program was designed to provide an experimental data base in order to determine the reflood phenomena as a function of the next parameters:

- flooding rate;
- system pressure;
- subcooling;
- initial cladding temperature and radial temperature distribution;
- rod power level and radial power distribution.

The range of test conditions and parameters studied during the experimental program is shown in Table 2.1. The complete test matrix comprises 48 experiments and is shown in Table 2.2.

2.5. Selected experiments

Out of the test matrix as shown in Table 2.2, 7 experiments have been selected for purpose of code assessment. Those selected experiments are presented in Table 2.3. Selection of the experiments is based on both the parameter variations being used for the various experiments, and the different physical phenomena being observed.

The data present in Tables 2.2 and 2.3 originates from ref. [2]. However, in order to perform the code assessment work as accurate as possible, more precise initial conditions have been obtained from the available data tapes. These latter initial conditions have been summarized in Table 2.4.

Table 2.1. Range of initial test conditions for the analyzed reflood experiments

Initial heater rod wall temperature	200°C - 850°C
Power	1.7 - 5 W/cm ²
Bundle outlet pressure (upper plenum pressure)	.2 - .6 MPa
Flooding rates:	
Constant	1.4 - 8.0 cm/sec
Variable in steps	3.0 - 0.9 cm/sec
Coolant subcooling	20°C - 80°C

Table 2.2. Test matrix for the ECN-reflood program

Exp. No.	(MPA)	T _{wall} initial, lev.4 (°C)			Power (W/cm ²)			V _{in} (cm/sec)	T _{in} (°C)
		c.r.	i.r.	o.r.	c.r.	i.r.	o.r.		
3215	.6	200	200	200	3.3	3.6	3.6	1.5	80
3216	.2	-	-	-	3.4	3.7	3.6	-	40
3218	.6	-	-	-	3.3	3.6	3.6	-	140
3220	.2	-	-	-	1.7	1.8	1.8	.7	100
3221	-	-	-	-	4.0	2.2	1.8	1.3	-
3224	-	-	-	-	3.4	3.7	3.6	1.5	-
3229	-	-	-	-	4.1	2.9	2.2	1.4	-
3230	.2	200	200	200	3.4	3.7	3.6	1.1-0.9	100
3231	-	-	-	-	3.4	3.7	3.6	1.7-0.9	40
4100	.2	600	600	600	3.3	3.6	3.5	8.0	100
4102	-	-	-	-	3.3	3.6	3.5	5.0	-
4106	-	-	-	-	3.6	3.6	3.5	2.4	-
4113	-	-	-	-	3.8	3.6	3.5	-	40
4114	-	-	-	-	3.8	3.0	2.2	-	-
4115	-	-	-	-	3.8	2.2	1.4	-	-
4116	-	-	-	-	3.8	3.0	2.1	-	100
4117	-	-	-	-	3.7	2.2	1.4	-	-
4118	-	400	400	400	3.6	3.6	3.5	-	-
4119	-	600	600	600	3.6	3.6	3.5	5.0	40
4120	-	-	-	-	3.6	3.6	3.6	8.0	-
4121	-	400	400	400	3.6	3.6	3.5	2.4	-
4122	-	600	600	600	1.9	1.7	1.7	-	-
4124	-	600	<	<<	3.6	2.2	1.4	-	-
4125	-	<<	600	600	0	3.6	3.5	-	-
4126	-	600	<	<<	3.6	2.2	1.4	8	-
4127	-	<<	600	600	0	3.6	3.5	-	-
4128	-	600	600	600	5.2	5.0	4.8	2.4	-
4129	-	-	-	-	4.8	5.0	4.8	8	-
4130	-	-	-	-	3.6	2.1	1.3	-	-
4131	-	600	<	<<	3.6	2.2	1.4	2.4	100
4132	-	<<	600	600	0	3.6	3.5	-	-
4133	-	-	-	-	0	3.6	3.5	8	100
4134	-	600	<	<<	3.6	2.2	1.4	-	-
4135	-	600	600	600	3.6	2.1	1.3	-	-
4136	-	-	-	-	5	5	5	2.4	100
4137	-	-	-	-	5	5	5	8	-
4138	-	800	800	800	3.6	3.6	3.6	2.4	-
4139	-	<<	800	800	0	3.6	3.6	-	-
4140	-	800	800	800	3.6	3.6	3.6	8	-
4141	-	<<	800	800	0	3.6	3.6	-	-
4142	-	800	800	800	3.6	3.6	3.6	2.4	40
4143	-	<<	800	800	0	3.6	3.6	-	-
4144	-	800	800	800	3.6	3.6	3.6	8	-
4145	-	<<	800	800	0	3.6	3.6	-	-
4146	.4	800	800	800	3.6	3.6	3.6	2.4	60
4147	-	-	-	-	3.6	3.6	3.6	8	-
4149	-	-	-	-	3.6	3.6	3.6	2.4	120
4150	-	-	-	-	3.6	3.6	3.6	8	-

c.r. = central rods
i.r. = inner ring rods
o.r. = outer ring rods

Table 2.3. Selected experiments

Experi- ment	Pres- sure (MPa)	Wall temp. (K)	Power (W/cm ²)			Inlet velocity (cm/s)	Inlet temp. (K)	Sub cooling (K)
			c.r.	i.r.	o.r.			
3216	0.2	473	3.4	3.7	3.6	1.5	313	80
3224	0.2	473	3.4	3.7	3.6	1.5	373	20
4100	0.2	873	3.3	3.6	3.5	8.0	373	20
4106	0.2	873	3.6	3.6	3.5	2.4	373	20
4120	0.2	873	3.6	3.6	3.6	8.0	313	80
4138	0.2	1073	3.6	3.6	3.6	2.4	373	20
4149	0.4	1073	3.6	3.6	3.6	2.4	393	23

c.r. = central rods

i.r. = inner ring rods

o.r. = outer ring rods

Table 2.4. Initial and operating conditions

EXP	P (MPa)	T _{in} (K)	t (s)	v _{in} (m/s)	Wall temperature (K)								t (s)	Power (W)	Power (W/cm ²)
					level										
					2	3	4	5	6	7	8				
3216	0.2	313	0	0	450	459	463	473	473	449	449	0	426.0	3.56	
			4.9	0								14.5	426.0		
			5.0	.15486								17.5	114805.3		
			805.0	.014356								587.5	115736.9		
3224	0.2	373	0	0	475	469	467	473	473	467	452	0	475	3.52	
			4.9	0								13.5	475.0		
			5.0	.014371								17.5	113668.6		
			1192.5	.014193								965.0	115347.2		
4100	0.2	373	0	0	899	893	893	873	865	863	846	0	8962.0	3.54	
			7.4	0								17.0	8962.0		
			7.5	.080549								20.5	114336.6		
			1000.0	.080549								398.0	115819.2		
4106	0.2	373	0	0	860	863	867	868	870	870	850	0	6505.0	3.48	
			7.4	0								6.0	6505.0		
			7.5	.023222								11.0	112308.7		
			1000.0	.023222								781.0	114510.7		
4120	0.2	313	0	0	849	851	859	857	860	859	841	0	6558.0	3.53	
			5.9	0								13.0	6558.0		
			6.0	.081754								16.0	113832.5		
			1000.0	.081754								131.5	115350.4		
4138	0.2	373	0	0	1105	1105	1114	1118	1122	1121	1095	0	18806.0	3.49	
			7.9	0								14.0	18806.0		
			8.0	.02349								19.0	112584.2		
			1000.0	.02349								409.0	114032.4		
4149	0.4	393	0	0	1082	1085	1104	1116	1115	1115	1083	0	10390.0	3.55	
			5.9	0								10.0	10390.0		
			6.0	.023123								14.0	112502.3		
			200.0	.023267								574.0	114565.7		
			380.0	.023275											
			766.0	.023273											

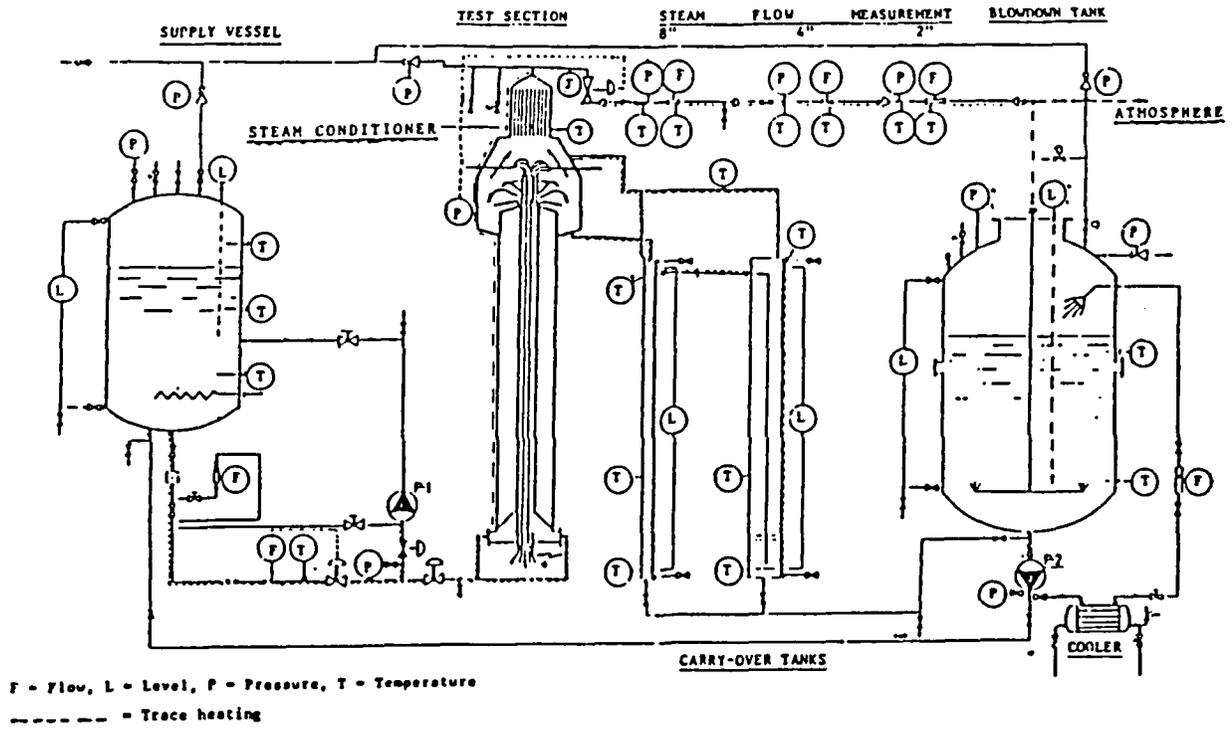


Figure 2.1. ECN-Reflood test facility schematics.

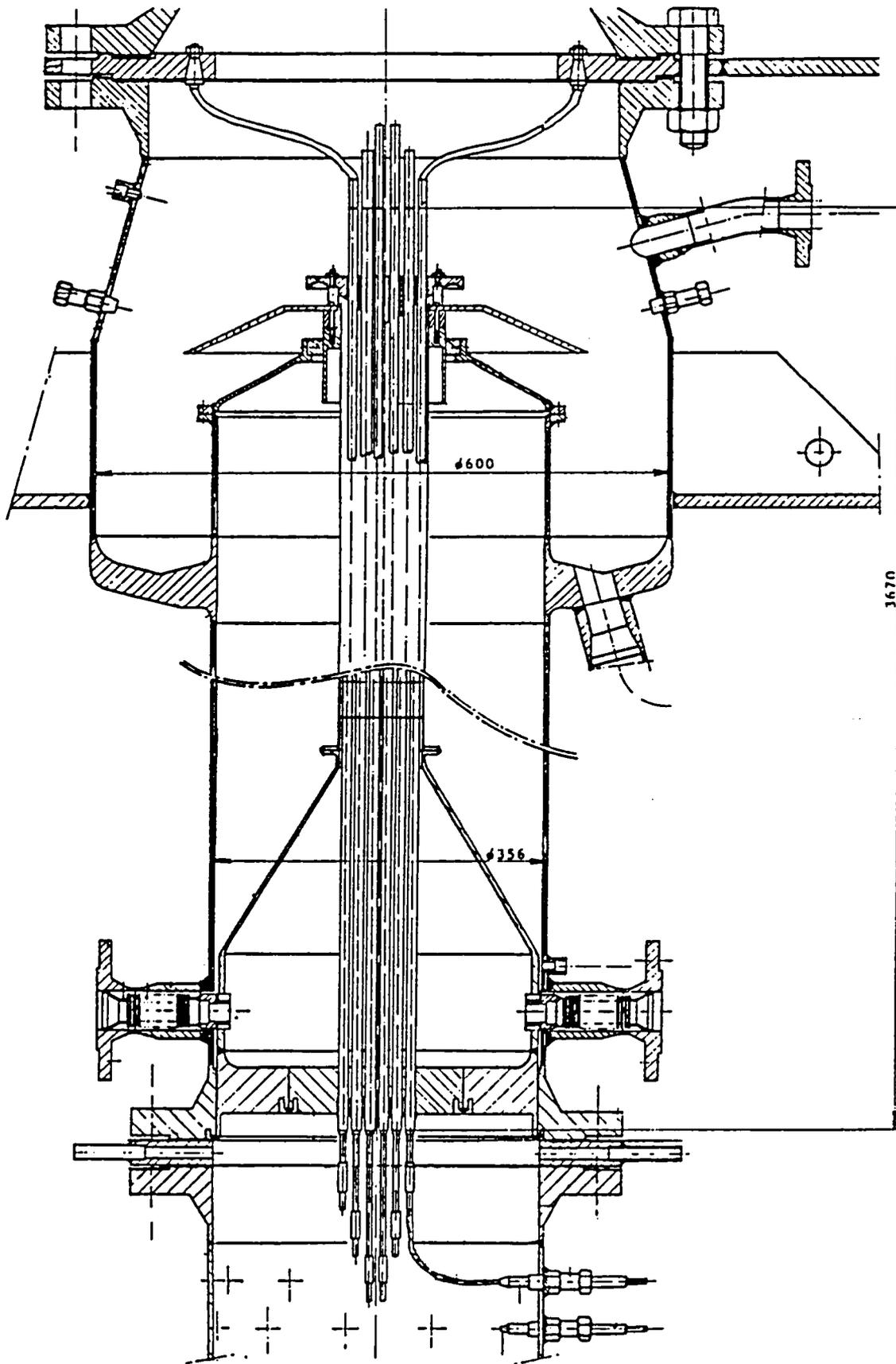
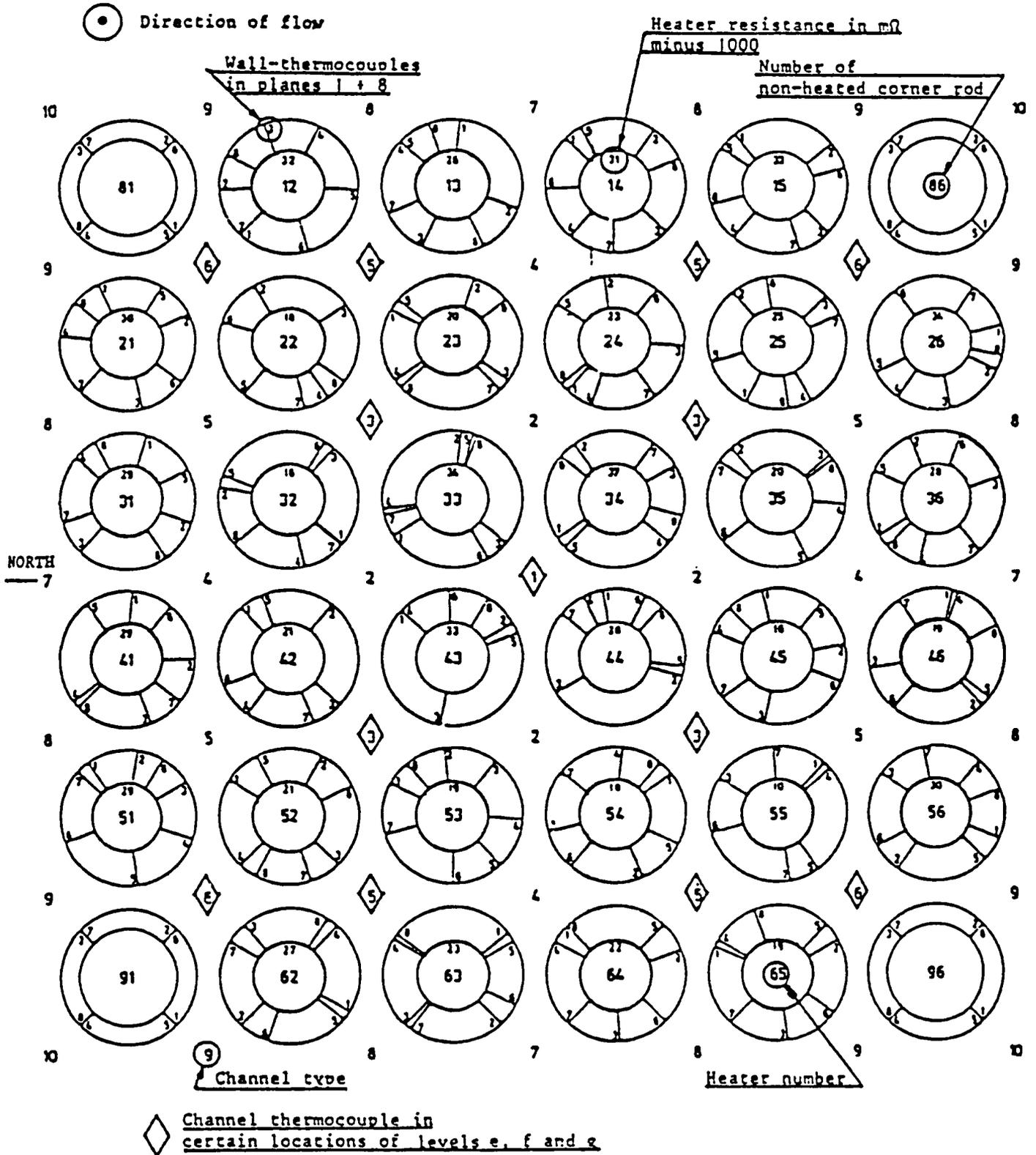


Figure 2.2. Test section and steam/water separator.



cross section area	47.8 cm^2	subchannel hydraulic diameter	13.6 mm
hydraulic diameter	12.5 mm	rod diameter	10.7 mm

Figure 2.4. Cross-section of the bundle with thermocouple positions.

3. CODE INPUT MODEL DESCRIPTION

The nodalization of the ECN 36-rod reflood test facility is quite simple. As indicated in Fig. 3.1 the electrically heated rod bundle is modelled as a pipe which is connected to a heat slab representing the heater rods. Mass flow, pressure and temperature of water entering the lower plenum of the test section are controlled by the time dependent junction 115 and the time dependent volume 110. Downstream of the test section, the steam water separator has been modelled with the RELAP5 separator component. The separator component is connected to the time dependent volumes 950 and 955.

3.1. Input model sensitivity analyses

Parameters for which a sensitivity analysis may be performed are the length of the hydrodynamic nodes and the maximum number of fine mesh intervals as applied by RELAP5/MOD2 to calculate the axial heat conduction in the rods when using the reflood model. User recommendations suggest a length of the hydrodynamic nodes between 0.15 and 0.61 m, and a maximum number of axial fine mesh intervals equal to 16 or 32. The maximum time step size should range between 0.01 and 0.05 seconds.

Four sensitivity analyses have been performed for experiment number 4100. The parameter variations studied are listed in Table 3.1. while the corresponding nodalization schemes are presented in Fig. 3.1. The resulting rod wall temperature time histories for levels 2 and 3 as identified in Fig. 2.3. are shown in respectively Figs. 3.2 and 3.3. As can be observed from these figures, run 1, 2, and 3 give approximately the same temperature behaviour. Run 4, in which volume lengths of 0.5 m have been used, deviates significantly from the previous three runs, but nevertheless comes closest to the experimentally determined temperature time histories. However, for purpose of determination of code uncertainty the nodalization of run 3 has been selected as the base case input model for code assessment. The temperature time histories as obtained for this run only differ to a minor extend from the ones resulting from run 1 and 2.

Furthermore, a hydrodynamic node length equal to 0.25 m as used in run 3 seems to be the lower bound with respect to core modelling for an actual nuclear power plant. RELAP5/MOD2 plant transient analyses using shorter length of the core hydrodynamic nodes will end-up in unacceptably high computer running times. The number of axial fine mesh intervals does not appear to influence the calculated temperature time histories significantly. Since a two times greater number of mesh intervals results in a small increase in computer running time, as will be shown in chapter 5, the finest mesh intervals will be used in the base case input model:

3.2. Base case input model

Based on the considerations as outlined in the previous section, the base case RELAP5/MOD2 input model nodalization is shown in Fig. 3.4. The hydraulic volumes have a length of 0.25 m and the number of axial fine mesh intervals equal to 32. The maximum time step size is fixed at 0.01 s.

3.3. Initial and operating conditions

The initial and operating conditions are presented in Table 2.4. The data have been fixed at these values by a careful examination of the available data tapes. In Appendix A the input decks for experiment 3216 are given for both the steady state calculation as well as the transient calculation (restart of the steady state calculation). The input decks for the other experiments can be obtained from Appendix A by replacing some data according to Table 2.4.

Table 3.1. Sensitivity analyses performed for experiment no. 4100

Run no.	Volume length (m)	Number of mesh intervals (-)	Maximum time step size (s)
1	.125	16	0.01
2	.125	32	0.01
3	.25	32	0.01
4	.50	32	0.01

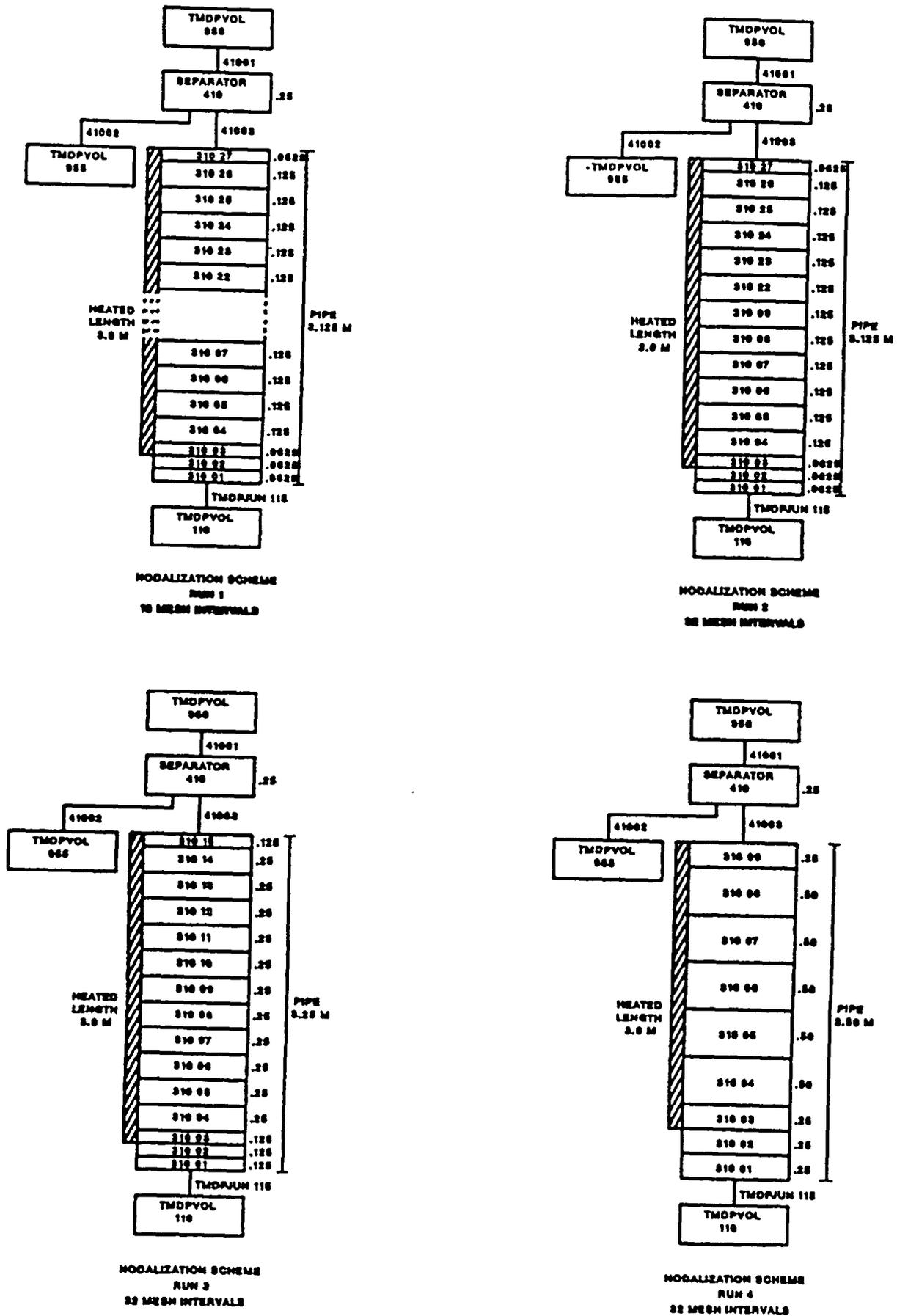


Figure 3.1. Nodalization schemes for sensitivity study.

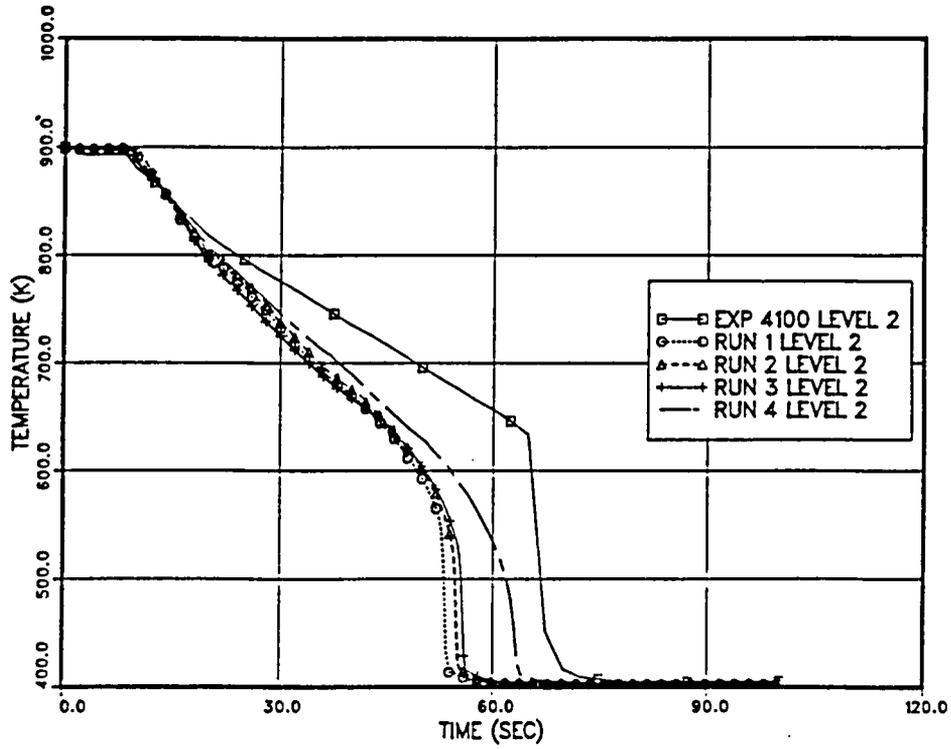


Figure 3.2. EXP 4100; Wall temperatures at level 2.

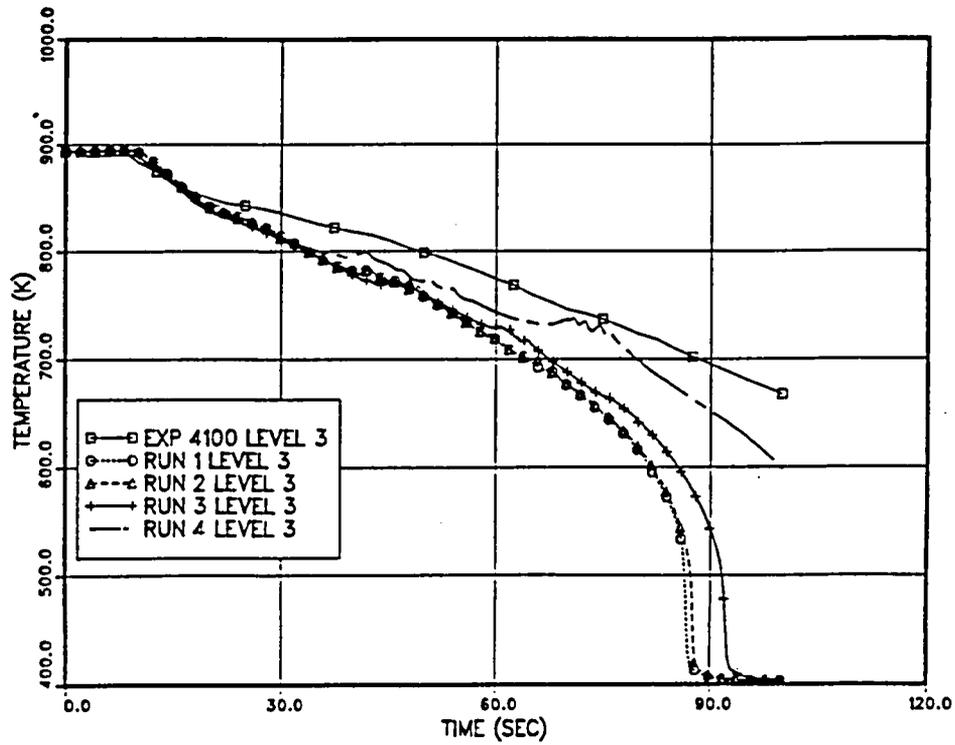


Figure 3.3. EXP 4100; Wall temperatures at level 3.

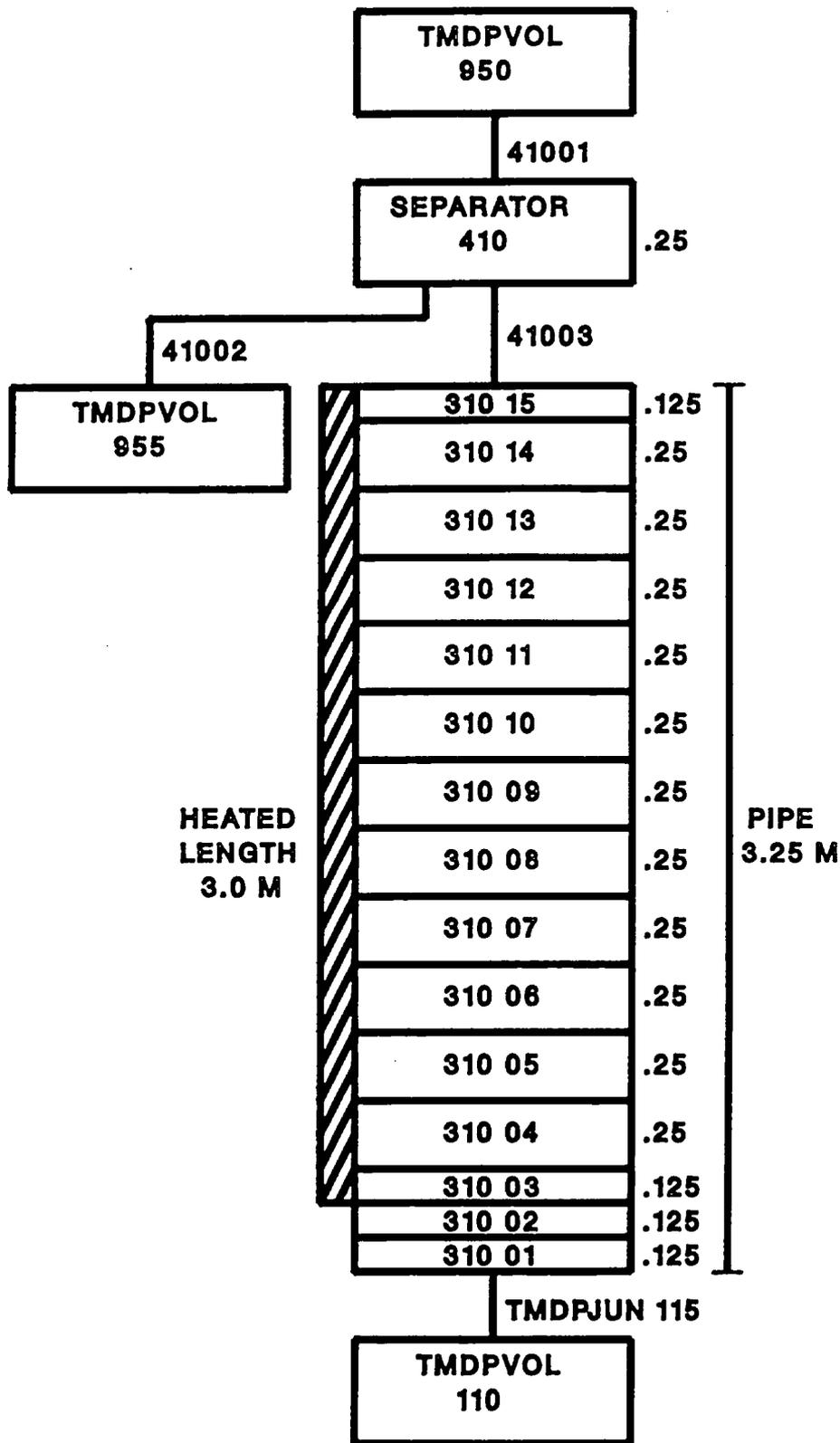


Figure 3.4.

NODALIZATION SCHEME

4. RESULTS

Comparisons between predictions with the code RELAP5/MOD2 and selected test data from the ECN-reflood experiments [2] are described below.

4.1. Sensitivity analyses

The results of the sensitivity analyses as described in chapter 3.1 can be summarized as follows:

- . The results of the coarse node model calculations (0.50 m) deviate significantly from the results obtained with the fine node model (0.125 and 0.25 m).
- . The number of axial fine mesh intervals (16 or 32) does not influence the calculated temperature time histories significantly as can be seen in Fig. 3.2 and 3.3.

Based on these conclusions the nodalization as presented in Fig. 3.4. is applied for the analyses.

4.2. RELAP5/MOD2 results vs experimental data

Code predictions are compared with the following measured quantities:

- . Integrated boundary mass flows.
- . Liquid mass inventory in the bundle.
- . Collapsed liquid level.
- . Quench front position.
- . Wall temperatures at different levels.

Comparisons between code predictions and test data for the seven selected reflood experiments are presented as follows:

- Experiment 3216: figures 4.1 - 4.8.
- Experiment 3224; figures 4.9 - 4.16.
- Experiment 4100; figures 4.17 - 4.24.
- Experiment 4106; figures 4.25 - 4.32.
- Experiment 4120; figures 4.33 - 4.40.
- Experiment 4138; figures 4.41 - 4.48.
- Experiment 4149: figures 4.49 - 4.56.

4.3. Analysis of results

The calculations have been performed with the code RELAP5/MOD2 using the available reflood model. As already mentioned in the previous section the number of axial mesh intervals during reflood is set to 16 and the nodalization presented in Fig. 3.4 is applied. The reflood model has to be activated at the start of each calculation. The reflood heat transfer package in the code RELAP5/MOD2, however, is only valid for flow patterns occurring at high reflood velocities (inverted annular flow). As for low reflood velocities a different flow pattern occurs (annular flow) a here-with corresponding heat transfer package should have been applied. For this reason agreement between calculated and experimental data can be expected for high reflood velocities. Only at these high reflood velocity conditions a flow pattern with the quench front below the collapsed liquid level will occur.

In Figs. 4.57 through 4.70 the RELAP5/MOD2 calculated and the experimental results concerning quench front position and collapsed liquid level are presented for the different selected cases.

Only for experiment 4120 the condition of a quench front below the collapsed liquid level is met as can be seen in Figs. 4.65 and 4.66. For this experiment the calculated values compare in general well with the experimental results as presented in Figs. 4.33 through 4.40.

Figs. 4.71 through 4.78 show the calculated and measured heat flux at axial level 5, 6, 7, and 8 for experiment 4120. These figures show that near the quench front the calculated heat flux is overpredicted and that well above the quench front the heat flux is underpredicted. This explains the overprediction of the wall temperatures below the quench front and the underprediction of the wall temperatures above the quench front as presented in Figs. 4.39 and 4.40. The approach of the quench front causes a faster wall temperature decrease in the calculation due to an overestimation of the heat transfer and so the heat flux. Except for level 8 the calculated wall temperatures for experiment 4100 show the same good agreement as described above for experiment 4120 (Figs. 4.23 and 4.24). This agrees well with the above stated simplification in the RELAP5/MOD2 reflood model concerning heat transfer and flow regime. Experiment 4120 as well as experiment 4100 have a high reflood velocity leading to the inverted annular flow regime identical to the model in RELAP5/MOD2.

The calculated wall temperatures for experiments 3216 and 3224 show a large deviation from the experimental data (Figs. 4.7 and 4.8 and Figs. 4.15 and 4.16). These experiments have a low reflood velocity and for that reason do not experience the inverted annular flow regime. For this reason the heat transfer is widely underpredicted. Poor comparison results are also obtained for experiment 4106, 4138, and 4149 where the quenching of the higher levels starts far too late or not at all. The calculated quenching of level 2 and 3 in these experiments is reasonably predicted. cFigs. 4.31 and 4.32, Figs. 4.47 and 4.48, and Figs. 4.55 and 4.56). For almost all calculations the liquid carry-over is grossly overpredicted and this results in an underprediction of the collapsed liquid level. The overprediction of the carry-over of the water at the bundle outlet is that an overprediction of the interphase drag in rod bundle geometries.

4.4. Suggestions for model improvements

As the reflood heat transfer package in the code RELAP5/MOD2 is only valid for flow patterns occurring at high reflood velocities (inverted annular flow) implementation of heat transfer correlations for other flow patterns (annular flow) during reflood is recommended. Most of the RELAP5/MOD2 assessment work indicates an overprediction of the carry-over due to an overprediction of the interfacial drag. This deficiency of the code is also demonstrated in these analyses. For this reason the introduction of a better correlation for the interfacial friction in the bubbly and slug flow regimes is suggested.

4.5. User guidelines

User recommendations in the RELAP5/MOD2 manual suggest a length of the hydrodynamic nodes between 0.15 and 0.61 m, and a maximum number of axial fine mesh intervals equal to 16 or 32. The recommended maximum time step size should range between 0.01 and 0.05 seconds. In the base case RELAP5/MOD2 input model for the presented reflood analyses the length of the hydrodynamic nodes is 0.25 m with a maximum number of 32 axial fine mesh intervals at the quench level. The maximum time step equals to 0.01 second.

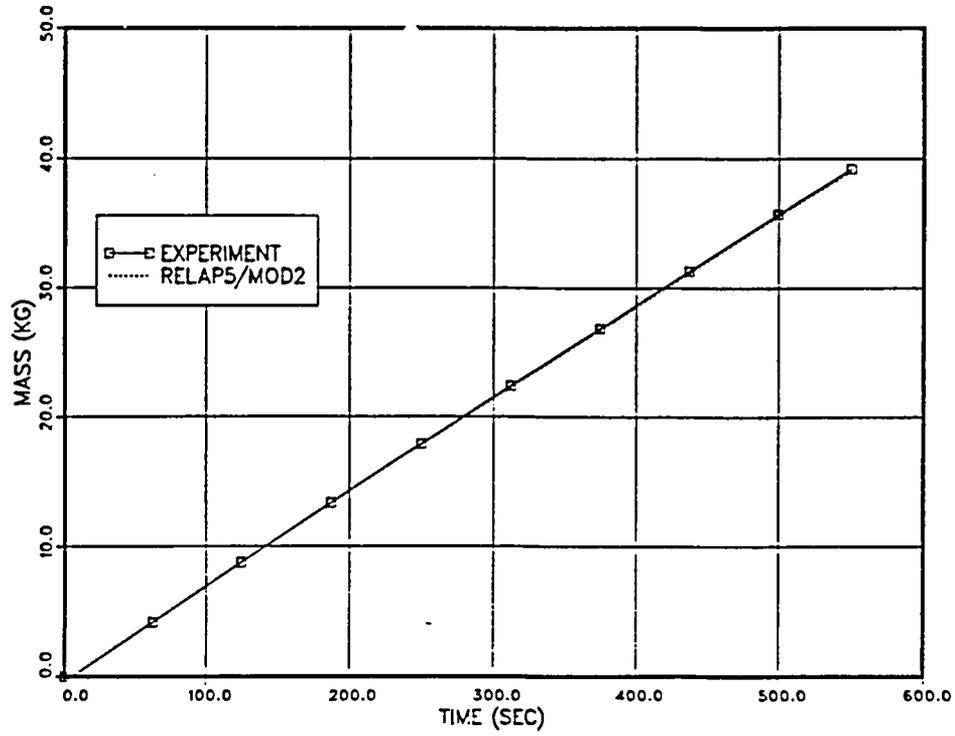


Figure 4.1. EXP 3216; Mass injected.

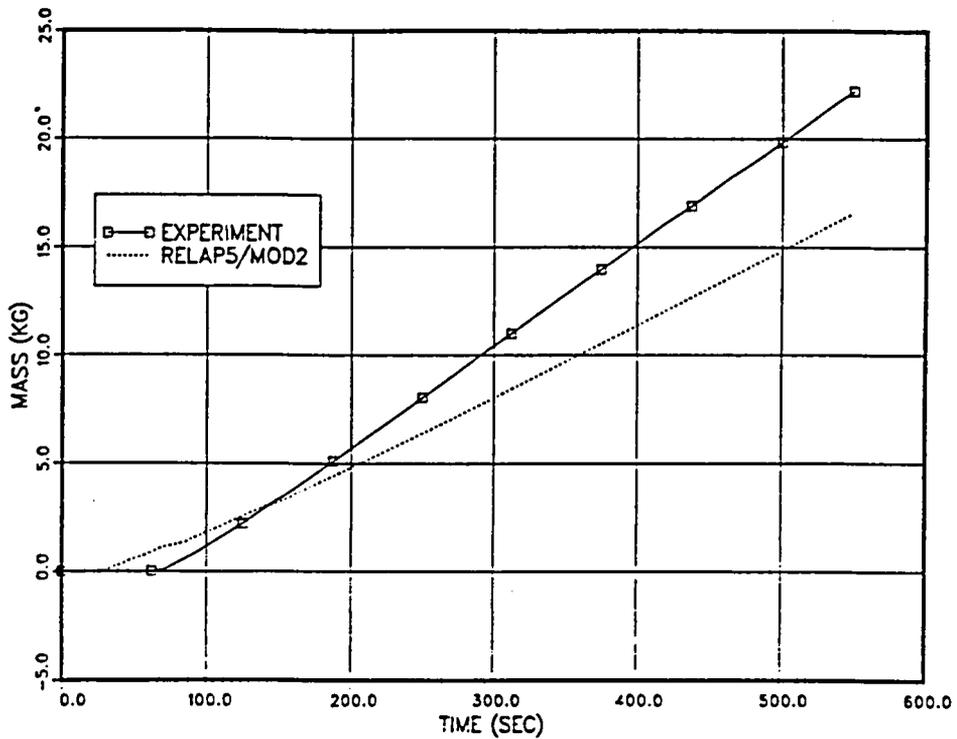


Figure 4.2. EXP 3216; Mass steam out.

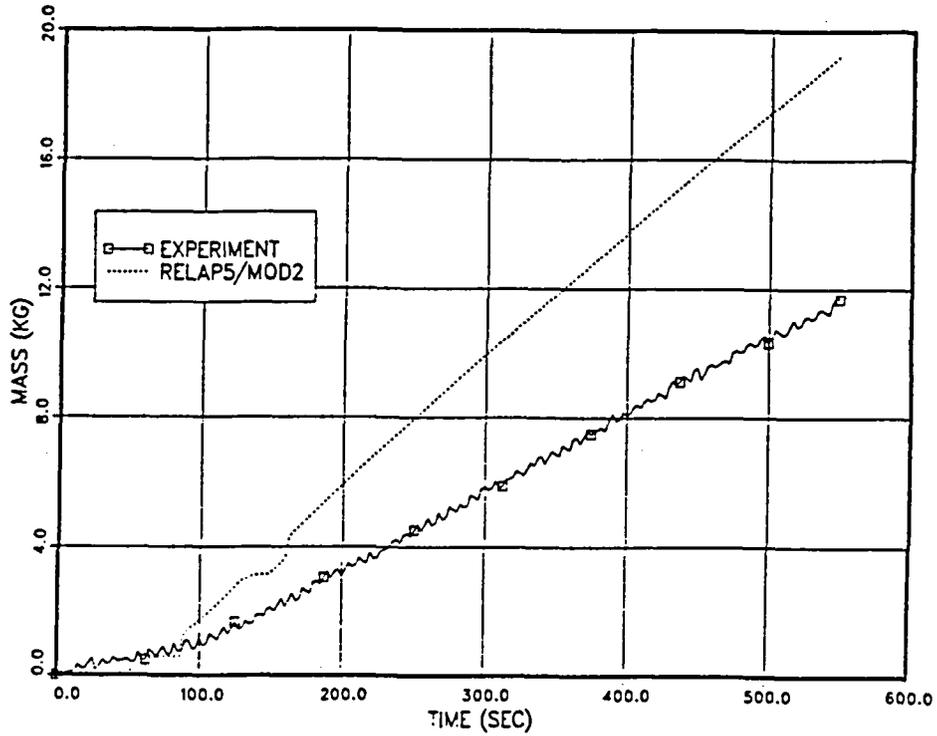


Figure 4.3. EXP 3216; Total mass carry-over.

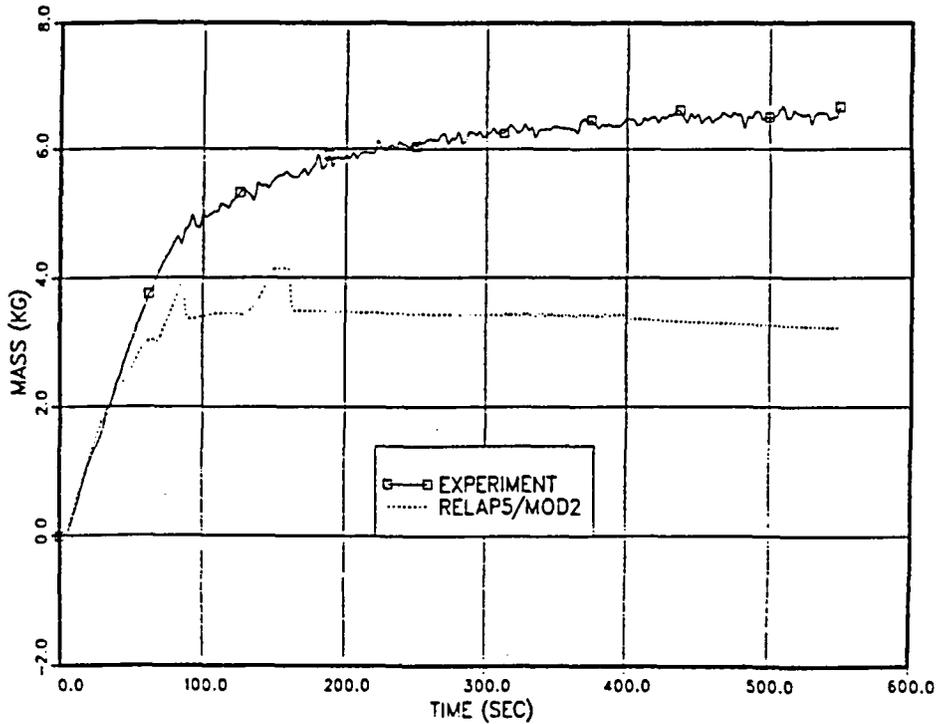


Figure 4.4. EXP 3216; Mass in the bundle.

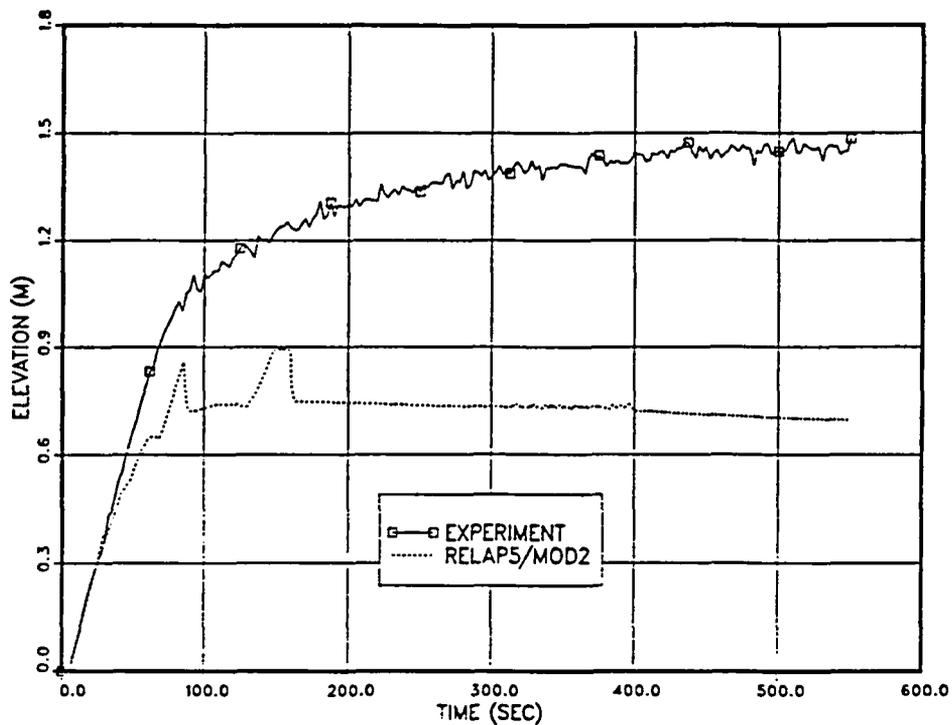


Figure 4.5. EXP 3216; Collapsed liquid level.

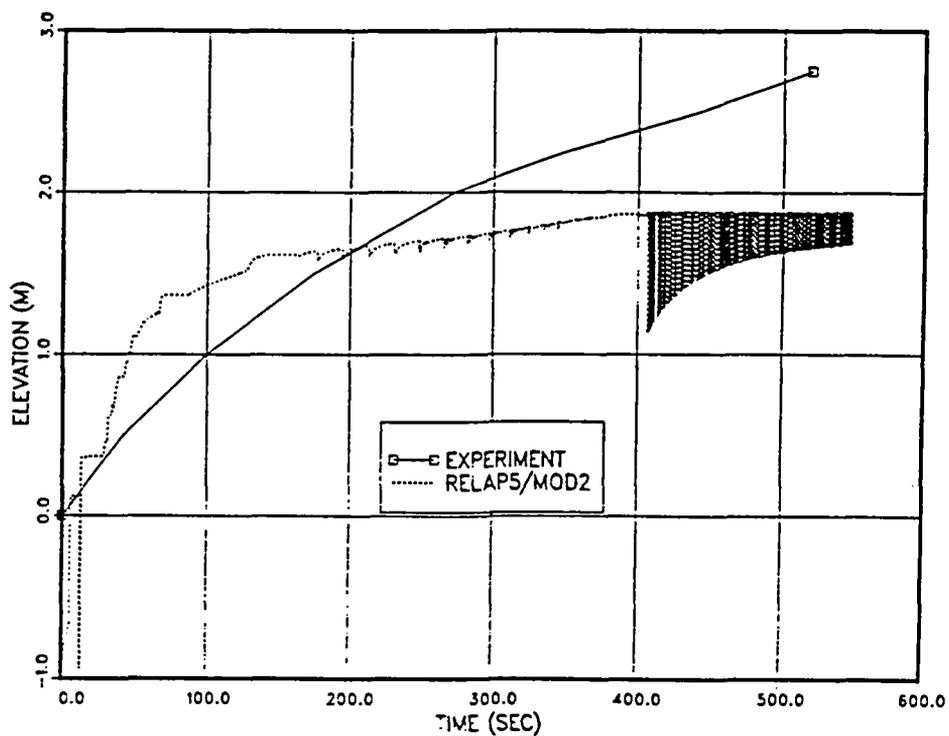


Figure 4.6. EXP 3216; Quench front position.

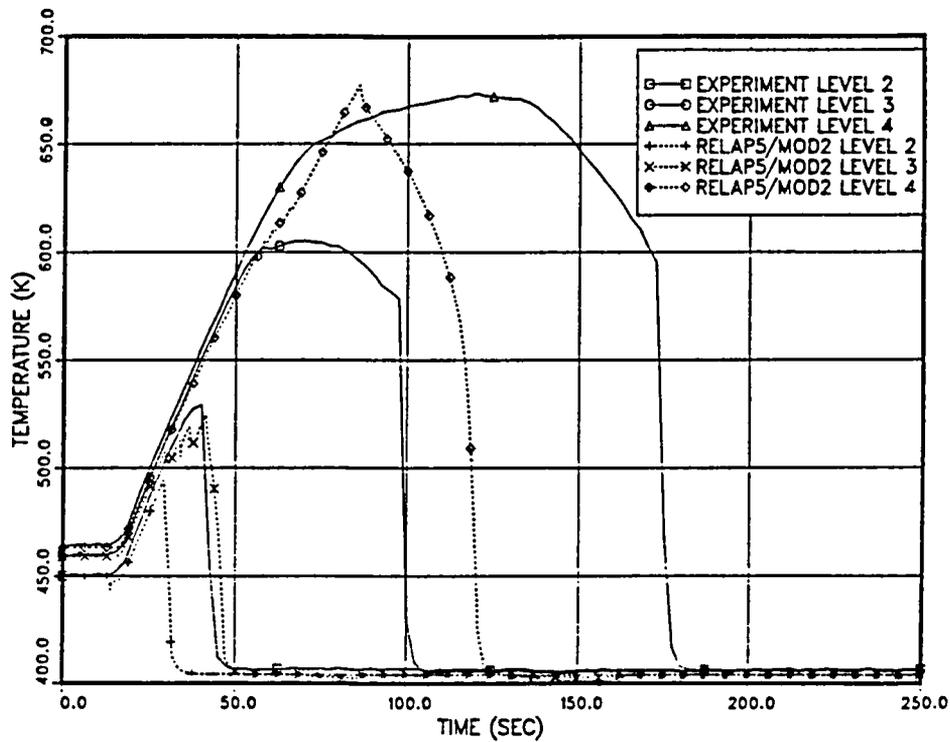


Figure 4.7. EXP 3216; Wall temperatures at level 2, 3, 4.

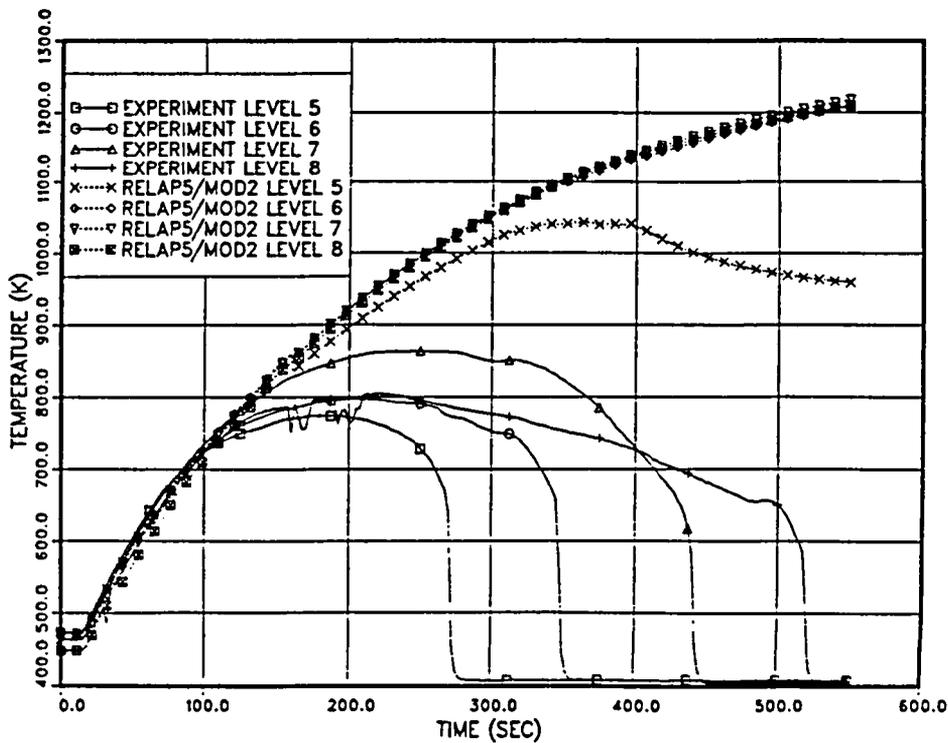


Figure 4.8. EXP 3216; Wall temperatures at level 5, 6, 7, 8.

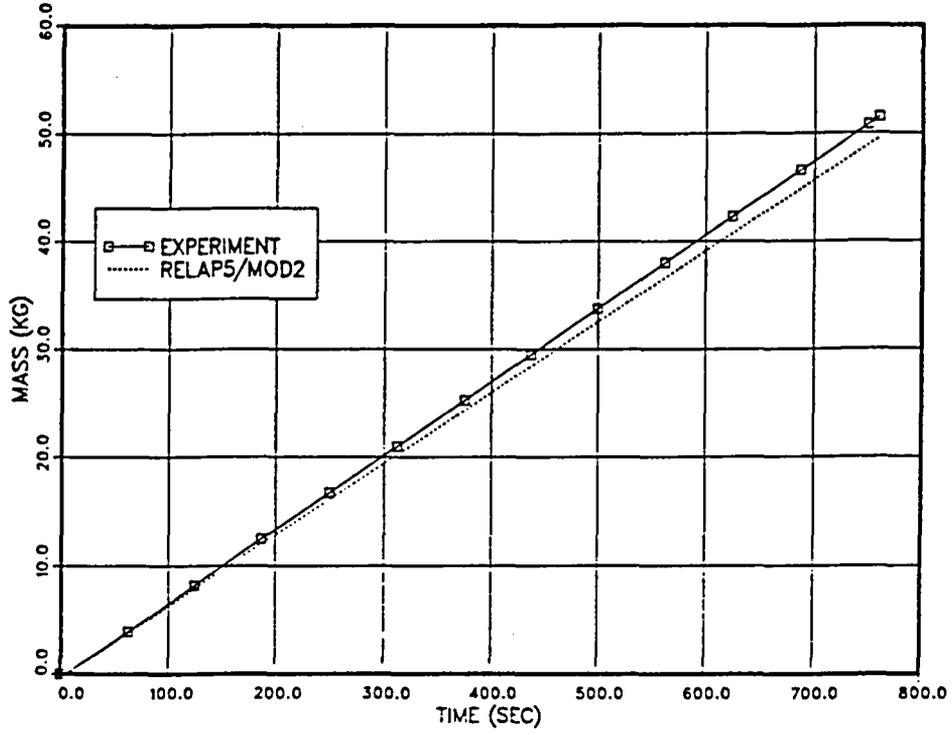


Figure 4.9. EXP 3224; Mass injected.

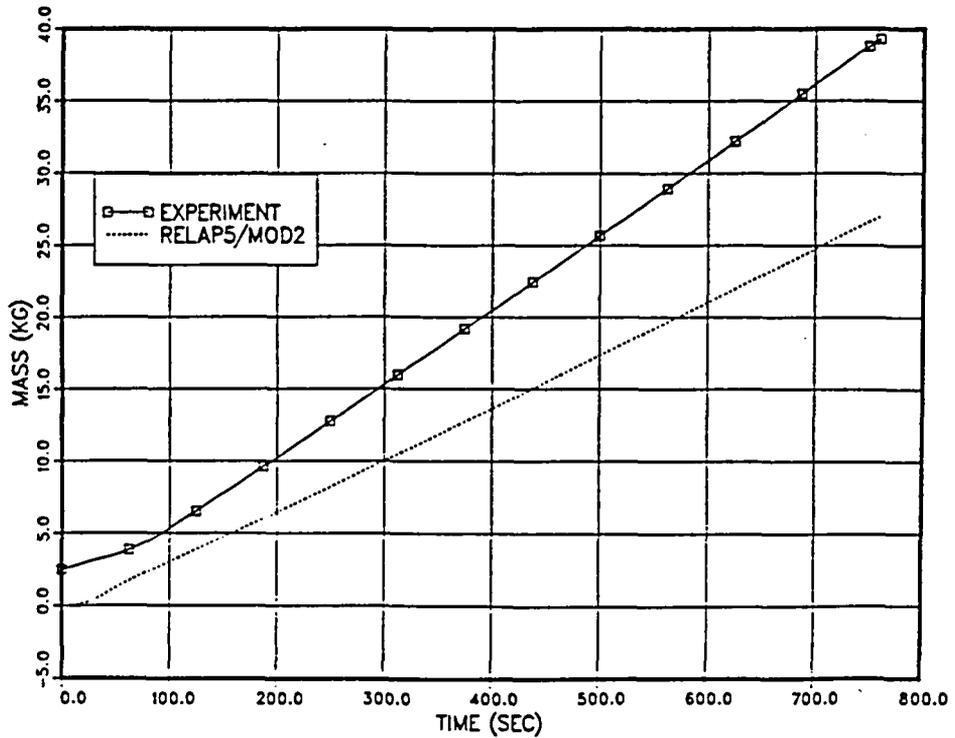


Figure 4.10. EXP 3224; Mass steam out.

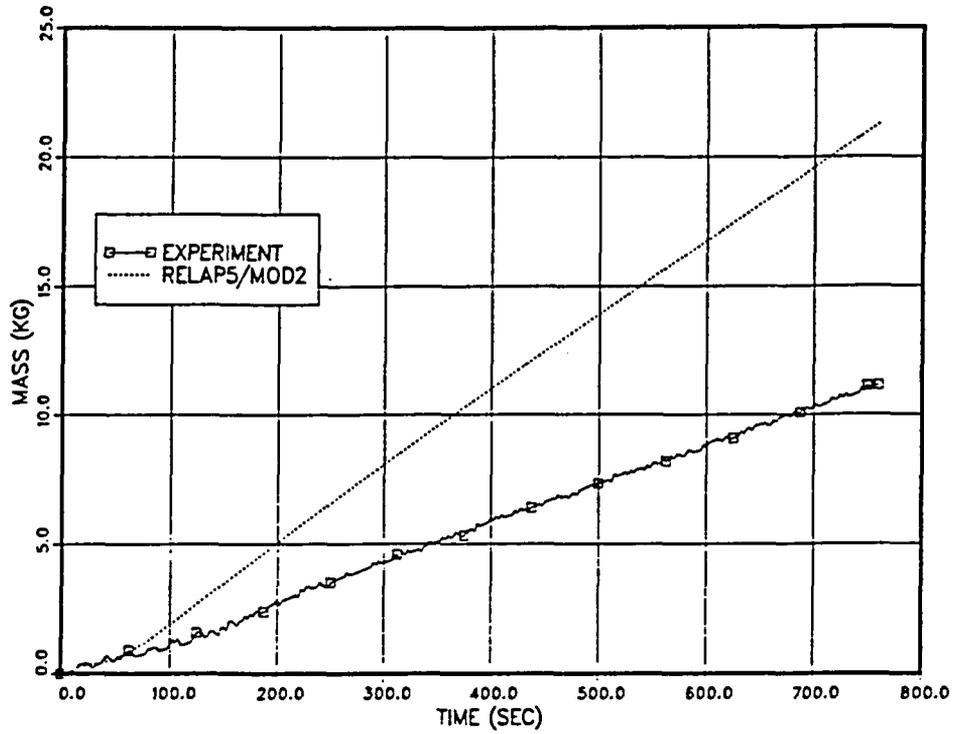


Figure 4.11. EXP 3224; Total mass carry-over.

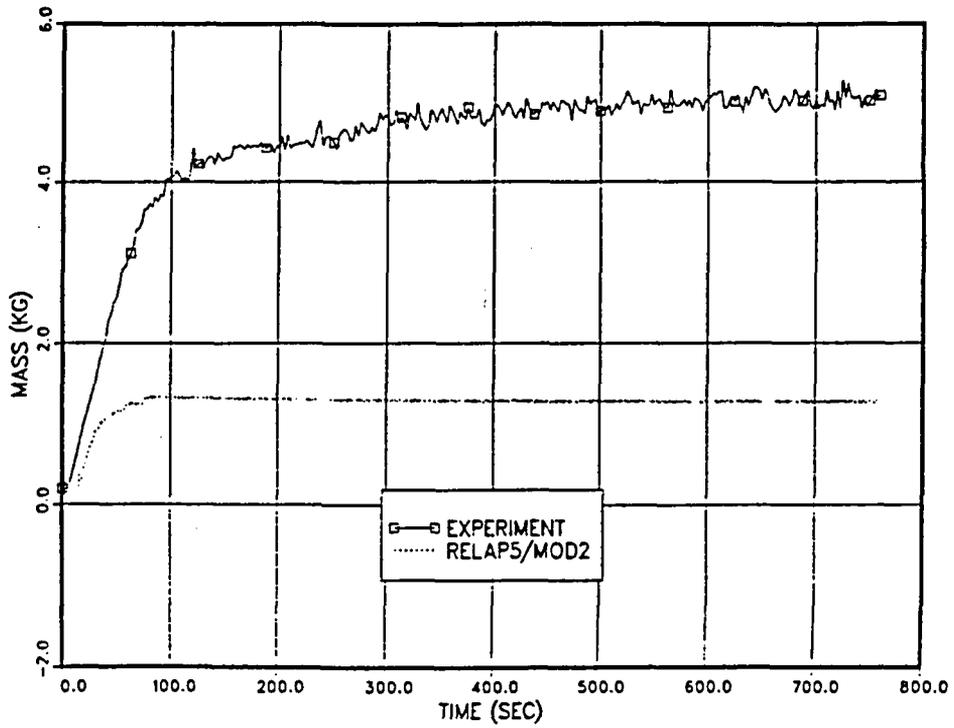


Figure 4.12. EXP 3224; Mass in the bundle.

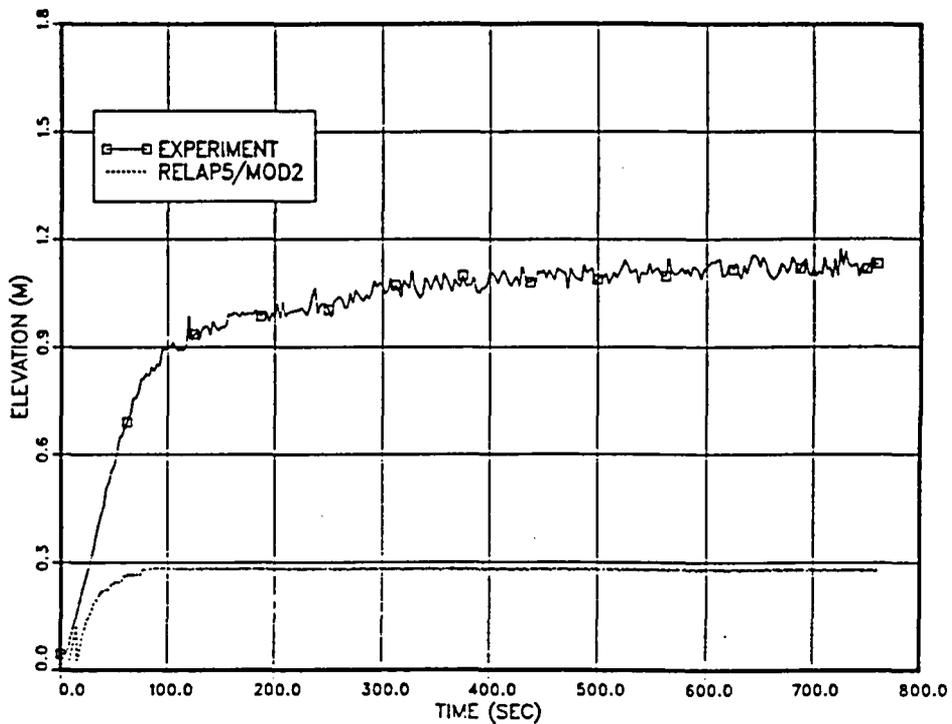


Figure 4.13. EXP 3224; Collapsed liquid level.

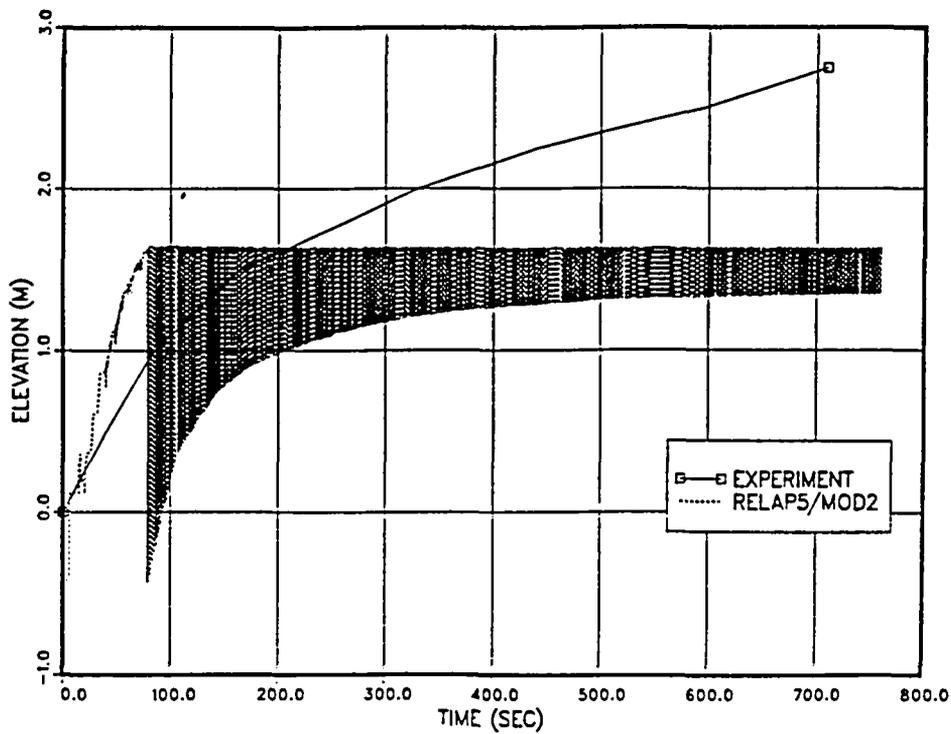


Figure 4.14. EXP 3224; Quench front position.

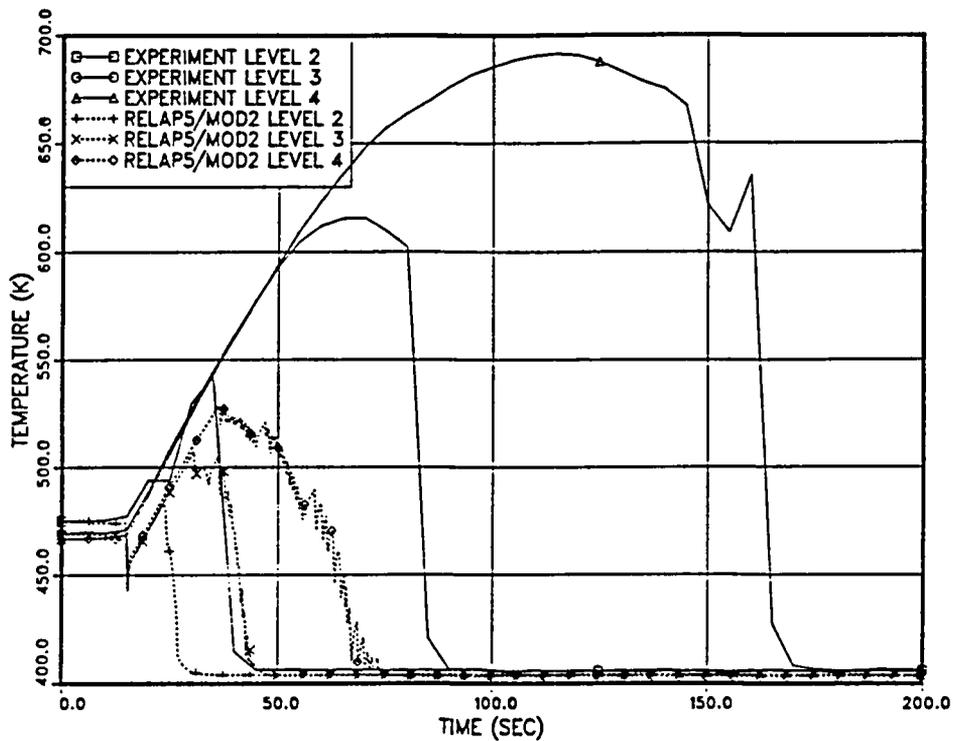


Figure 4.15. EXP 3224; Wall temperatures at level 2, 3, 4.

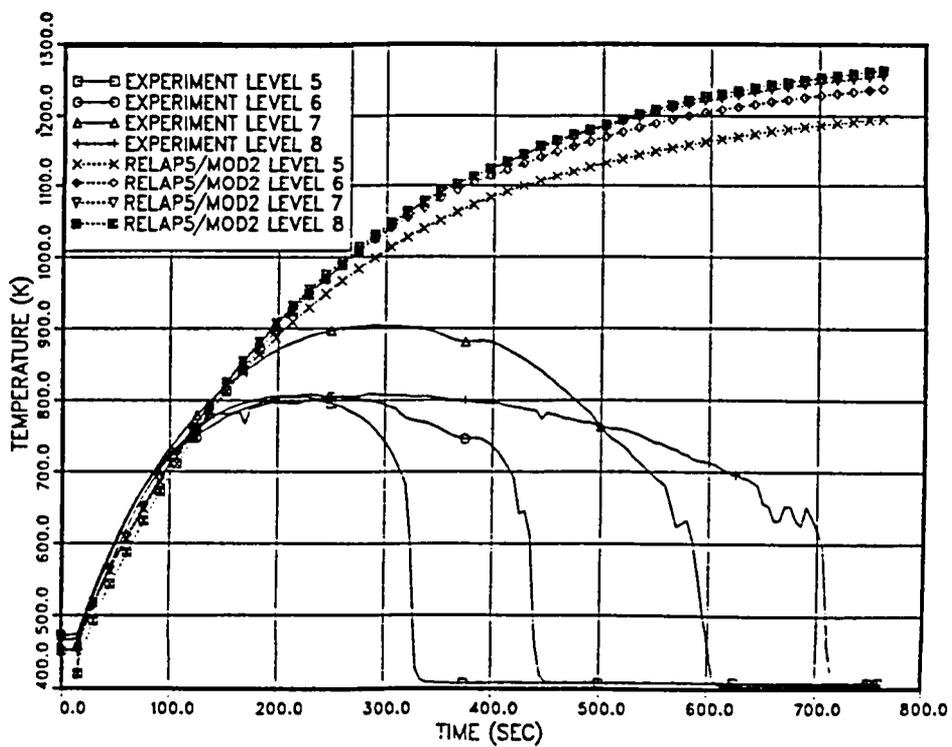


Figure 4.16. EXP 3224; Wall temperatures at level 5, 6, 7, 8.

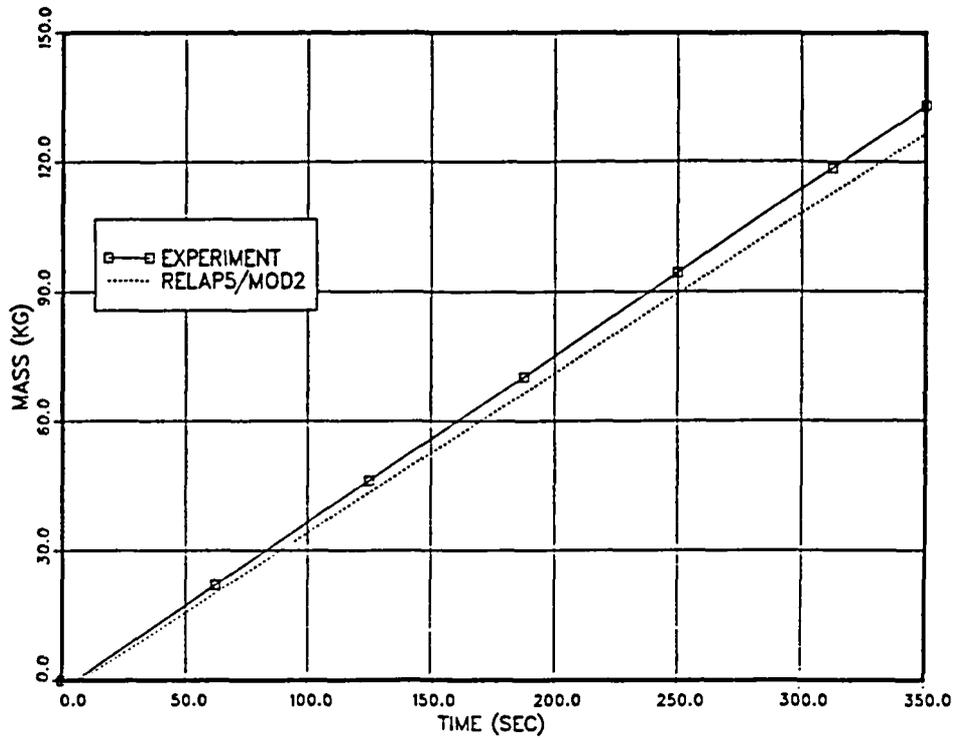


Figure 4.17. EXP 4100; Mass injected.

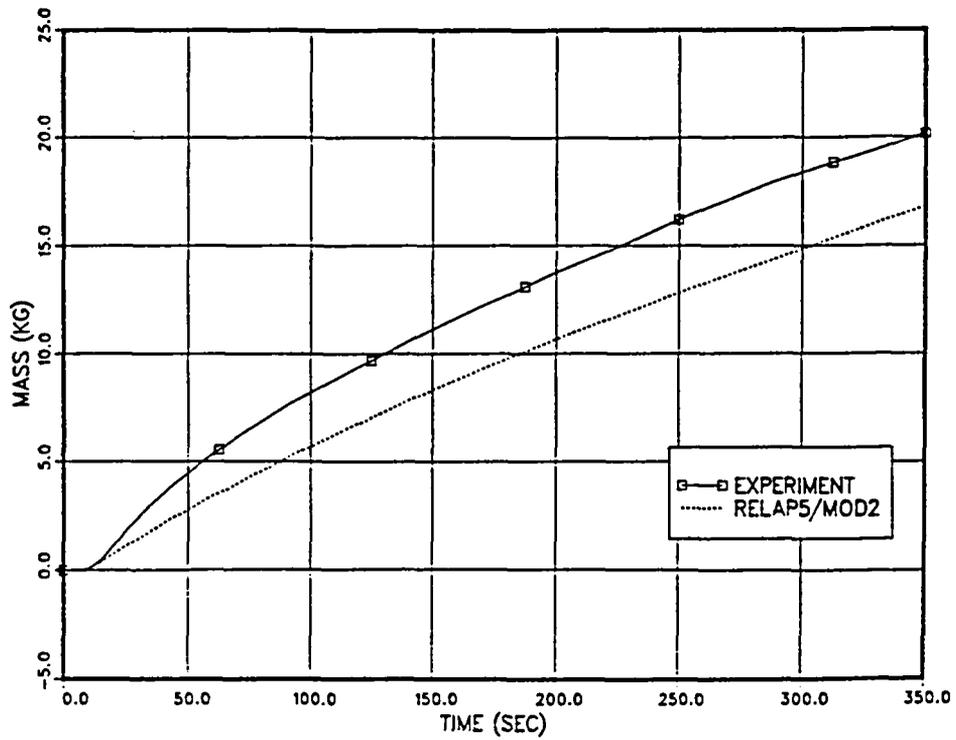


Figure 4.18. EXP 4100; Mass steam out.

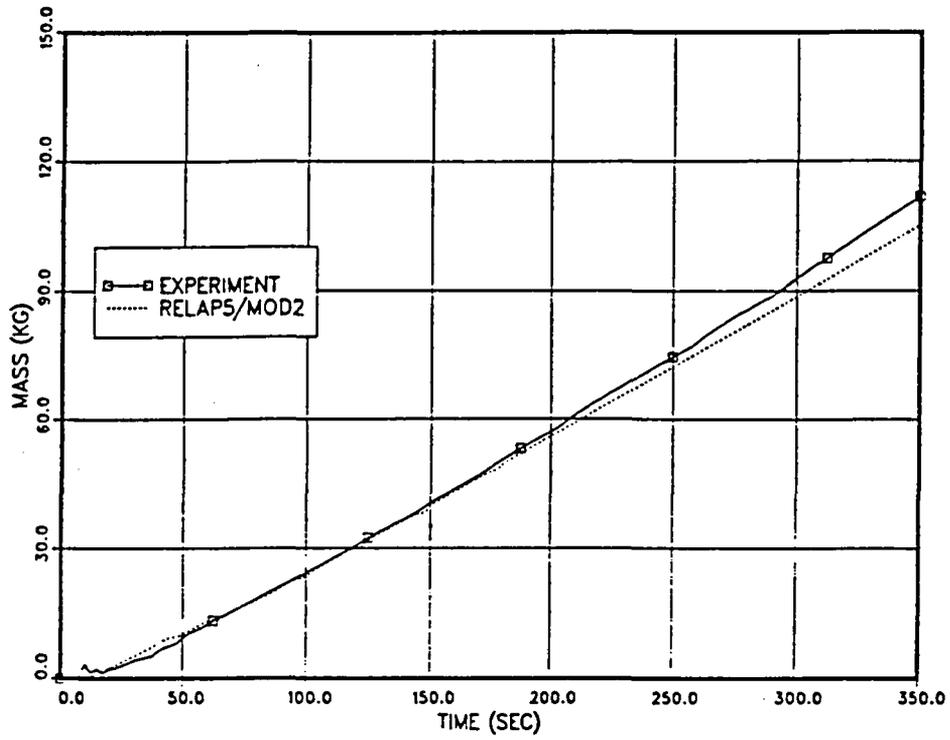


Figure 4.19. EXP 4100; Total mass carry-over.

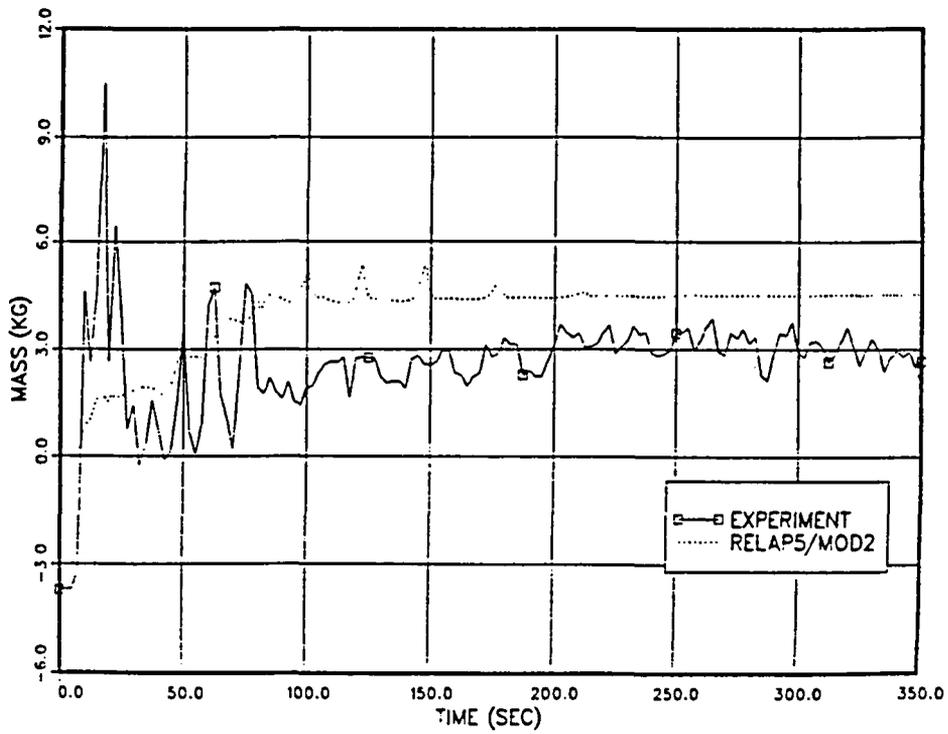


Figure 4.20. EXP 4100; Mass in the bundle.

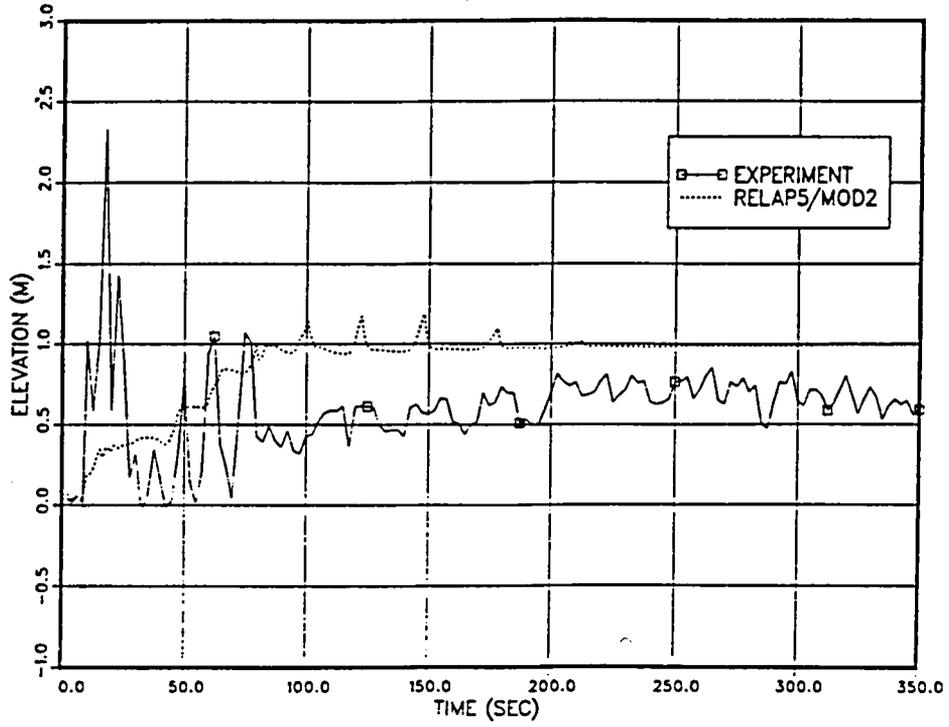


Figure 4.21. EXP 4100; Collapsed liquid level.

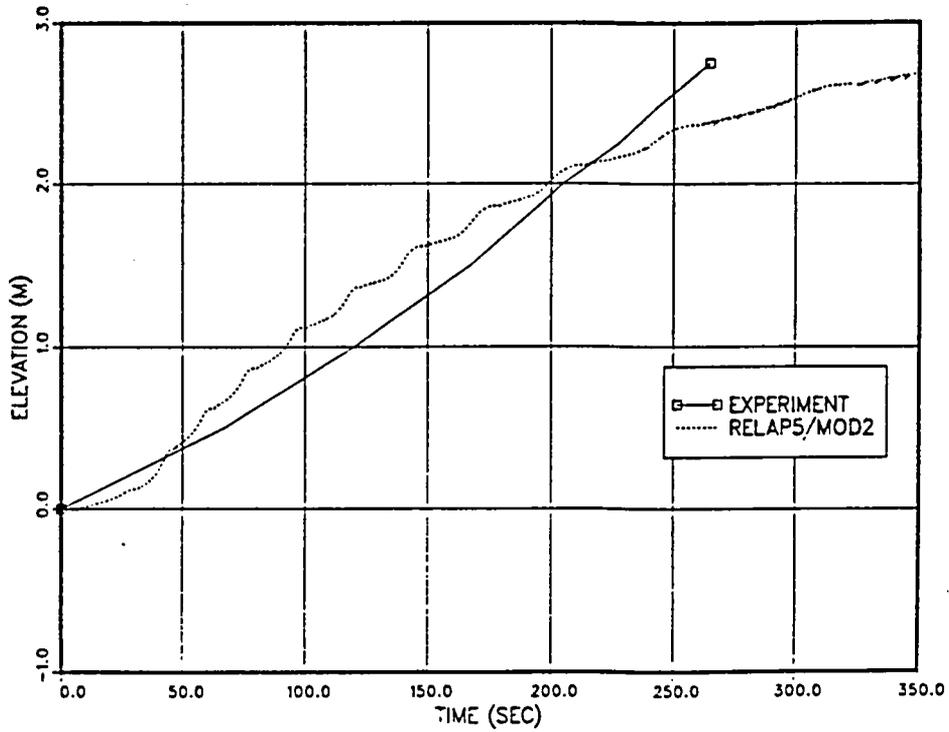


Figure 4.22. EXP 4100; Quench front position.

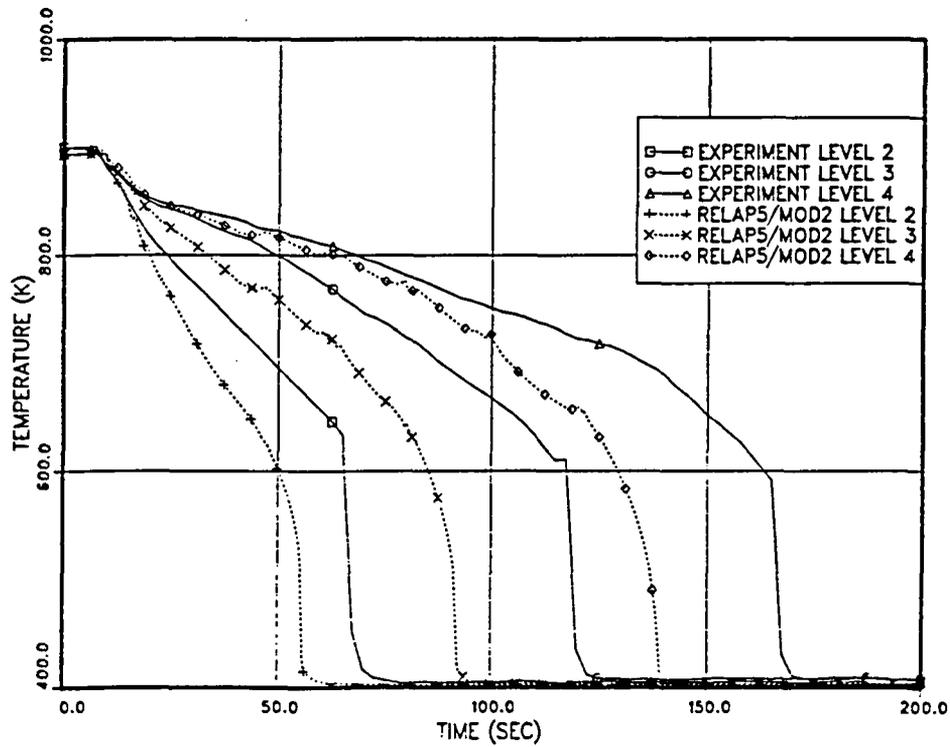


Figure 4.23. EXP 4100; Wall temperatures at level 2, 3, 4.

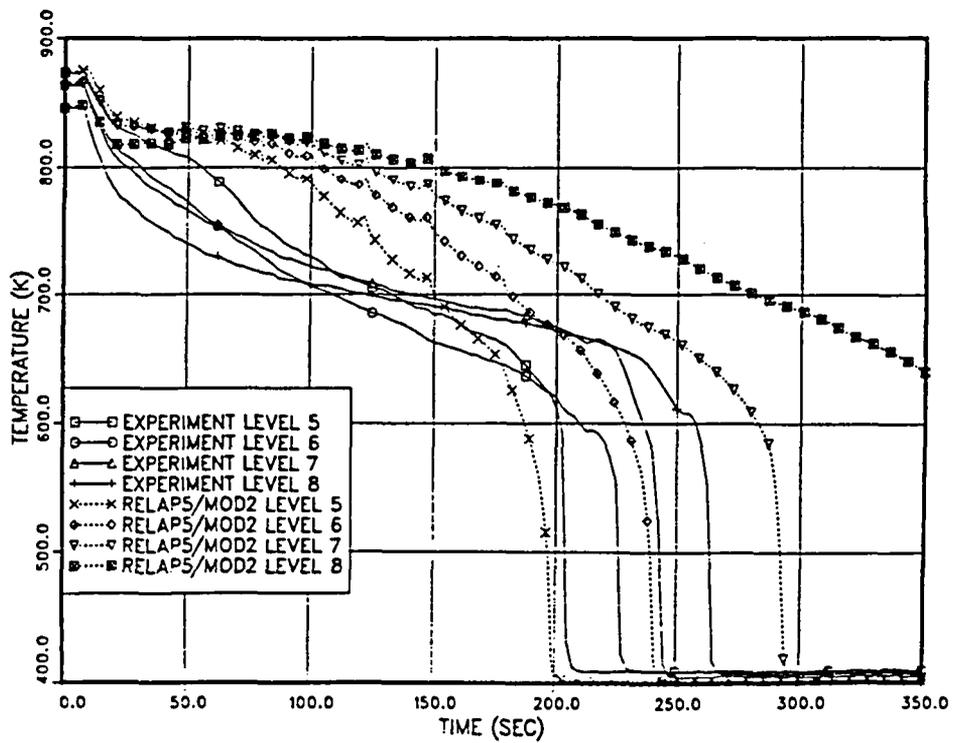


Figure 4.24. EXP 4100; Wall temperatures at level 5, 6, 7, 8.

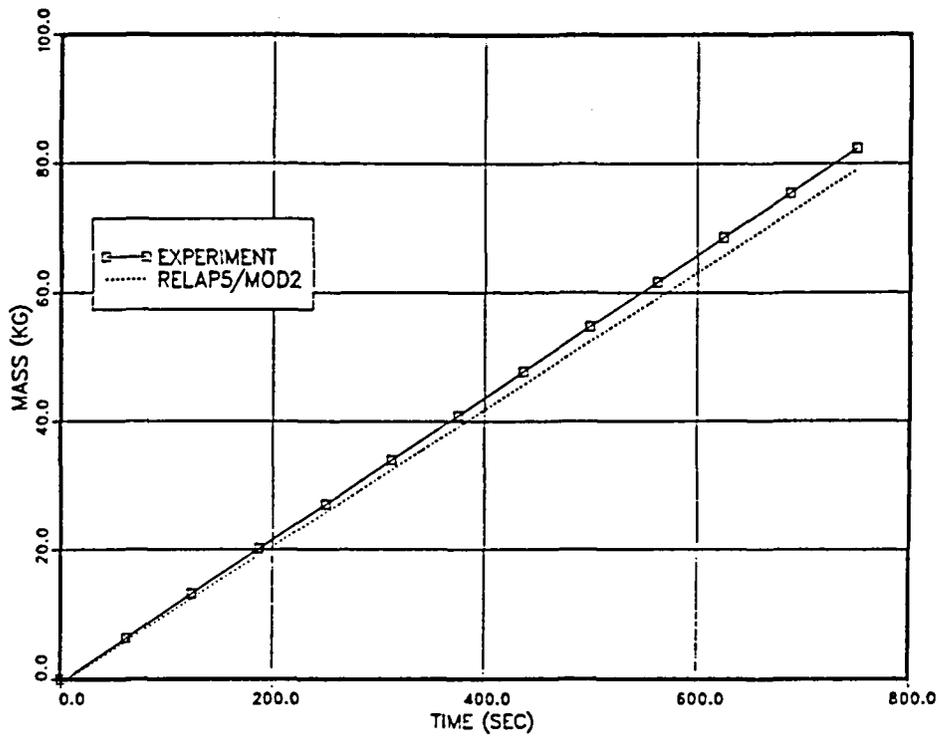


Figure 4.25. EXP 4106; Mass injected.

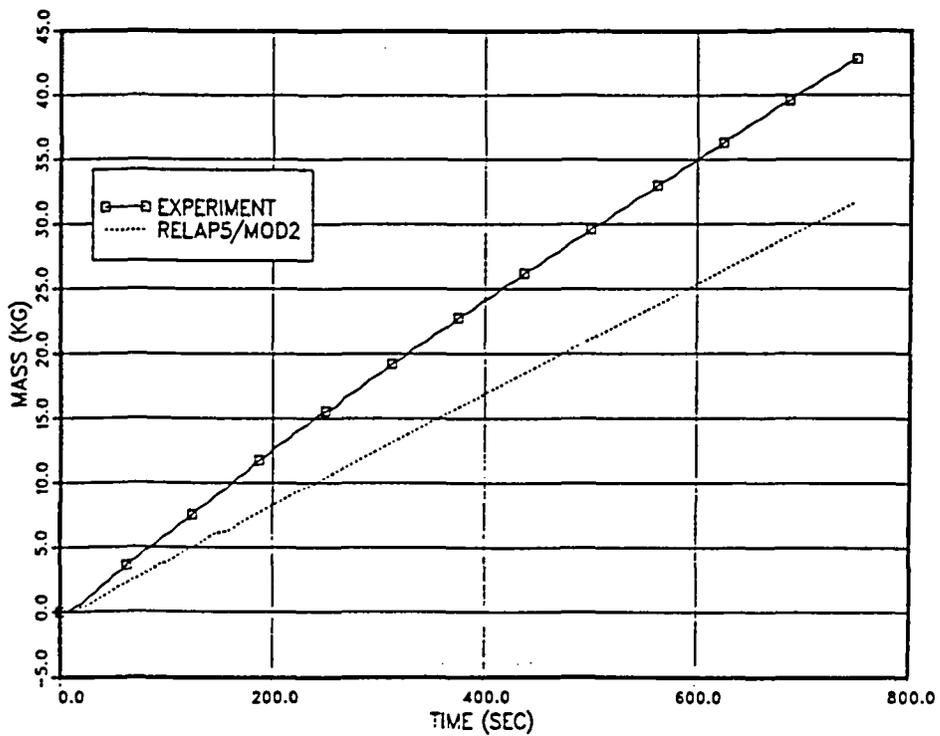


Figure 4.26. EXP 4106; Mass steam out.

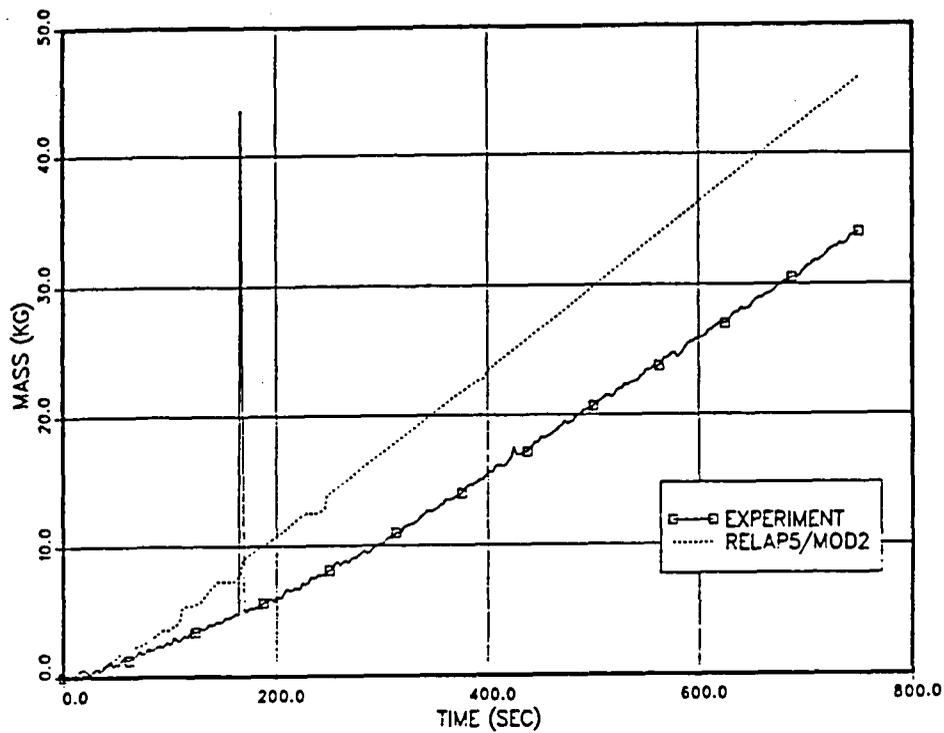


Figure 4.27. EXP 4106; Total mass carry-over.

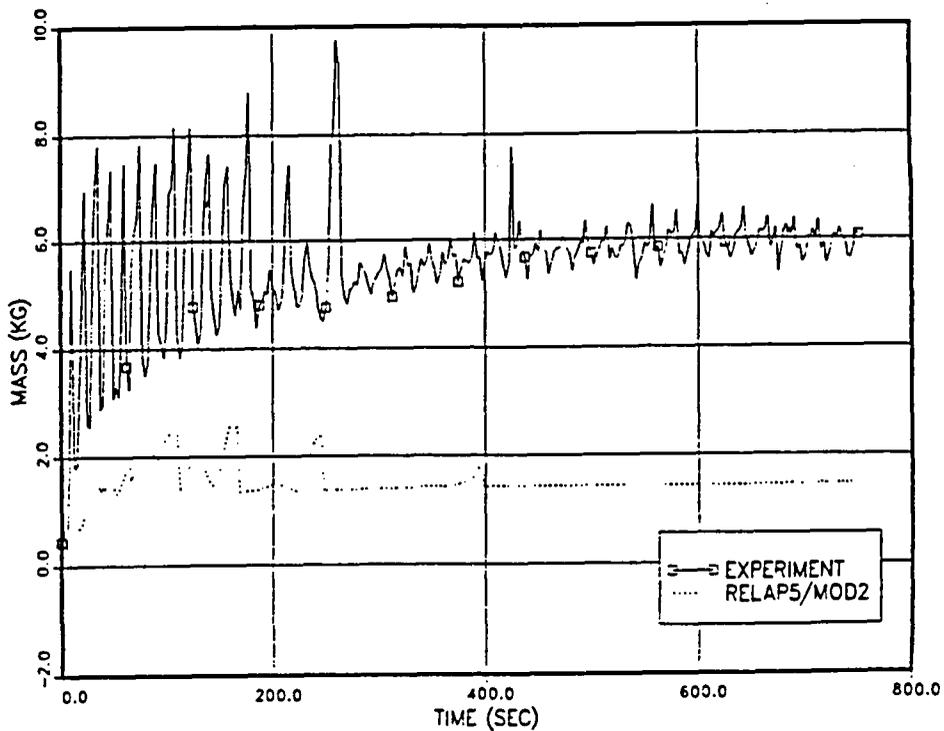


Figure 4.28. EXP 4106; Mass in the bundle.

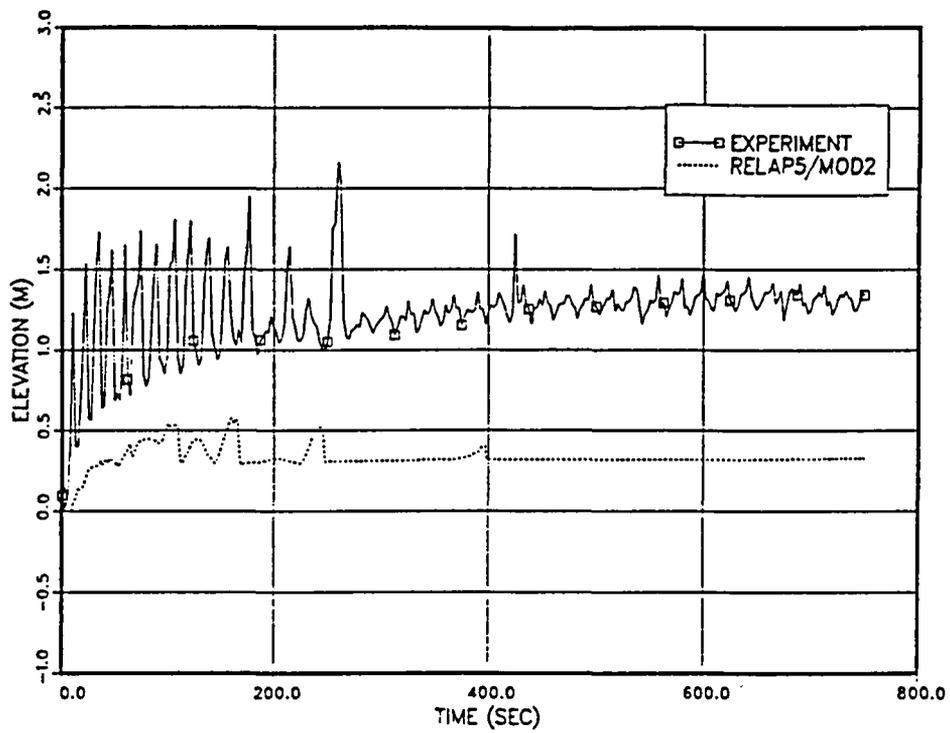


Figure 4.29. EXP 4106; Collapsed liquid level.

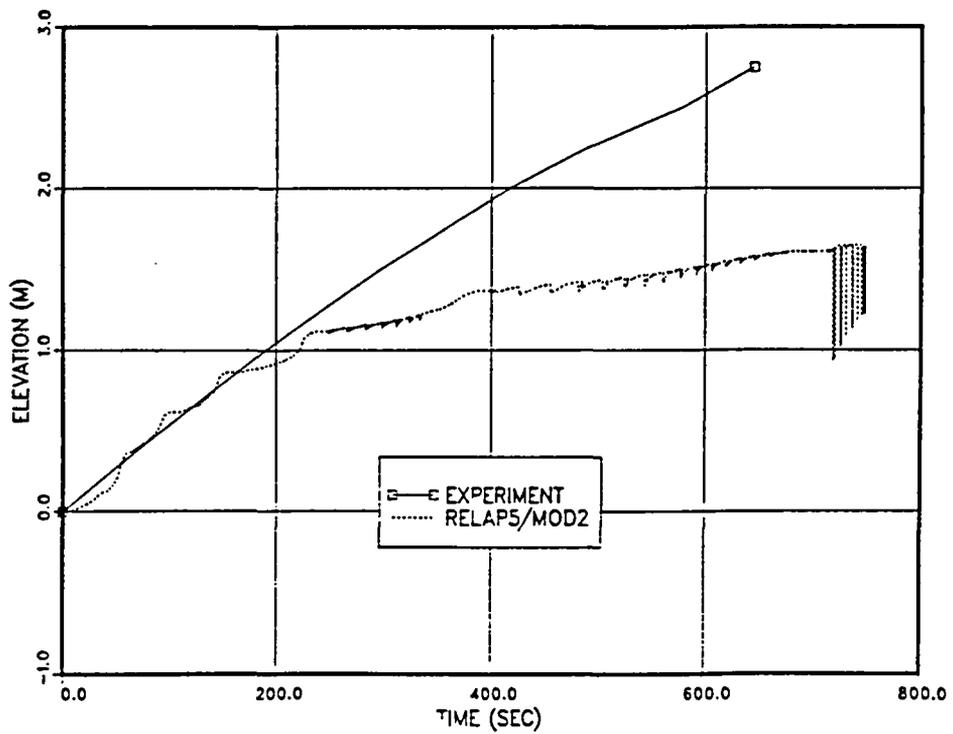


Figure 4.30. EXP 4106; Quench front position.

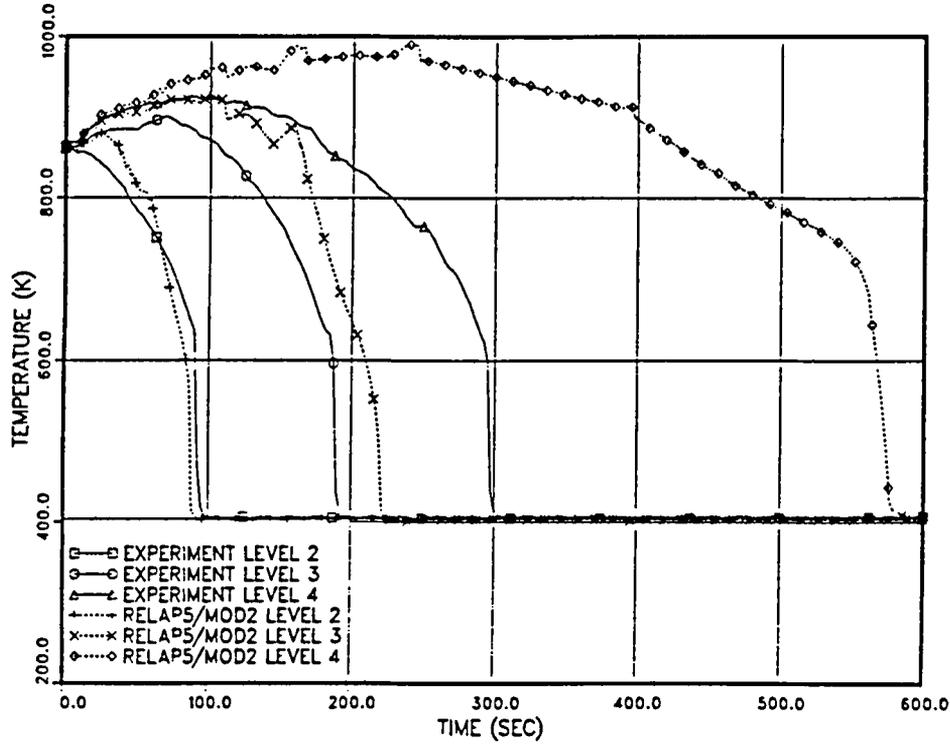


Figure 4.31. EXP 4106; Wall temperatures at level 2, 3, 4.

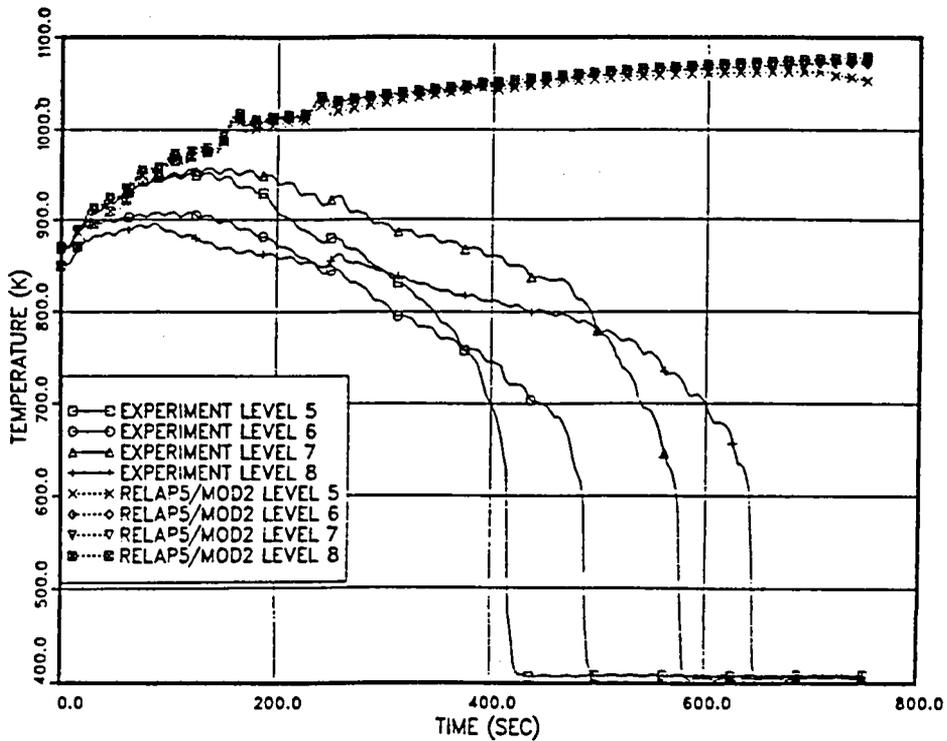


Figure 4.32. EXP 4106; Wall temperatures at level 5, 6, 7, 8.

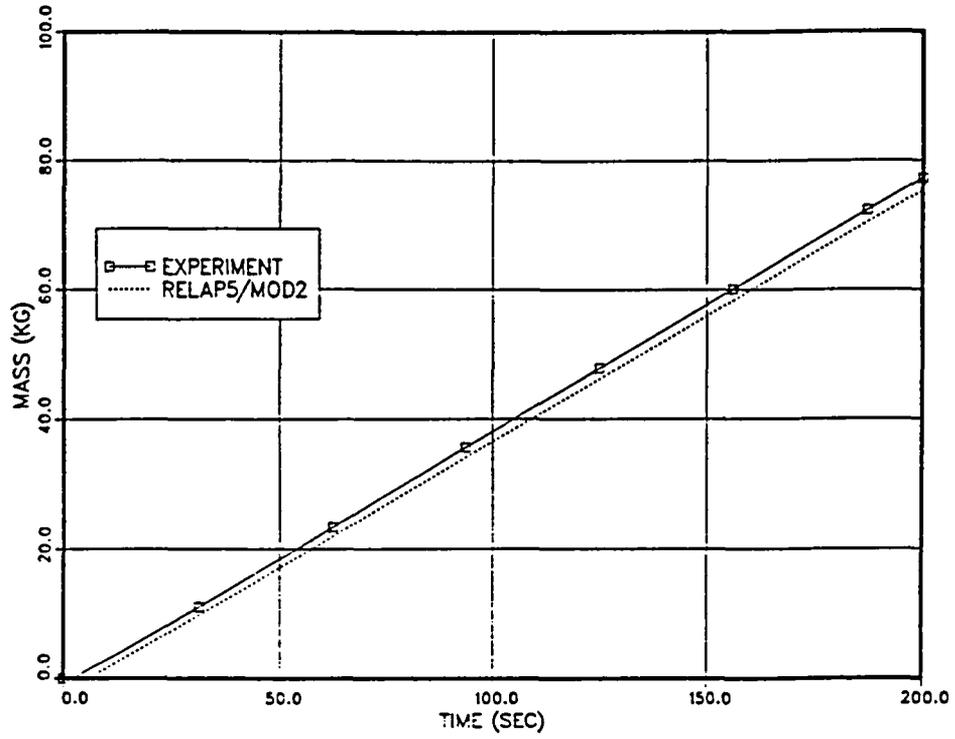


Figure 4.33. EXP 4120; Mass injected.

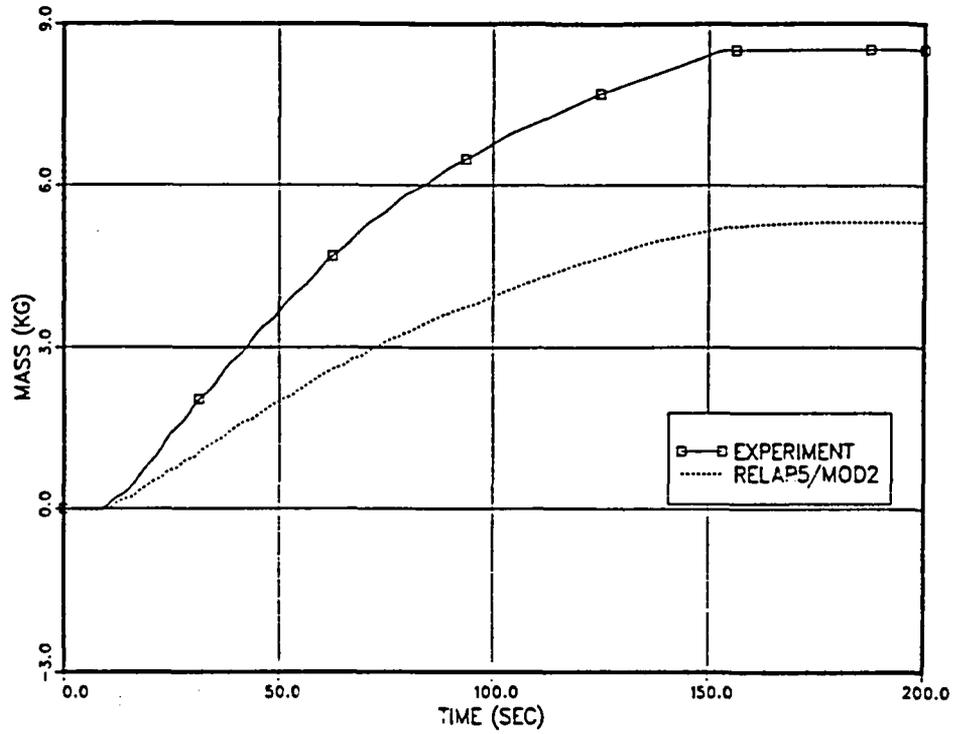


Figure 4.34. EXP 4120; Mass steam out.

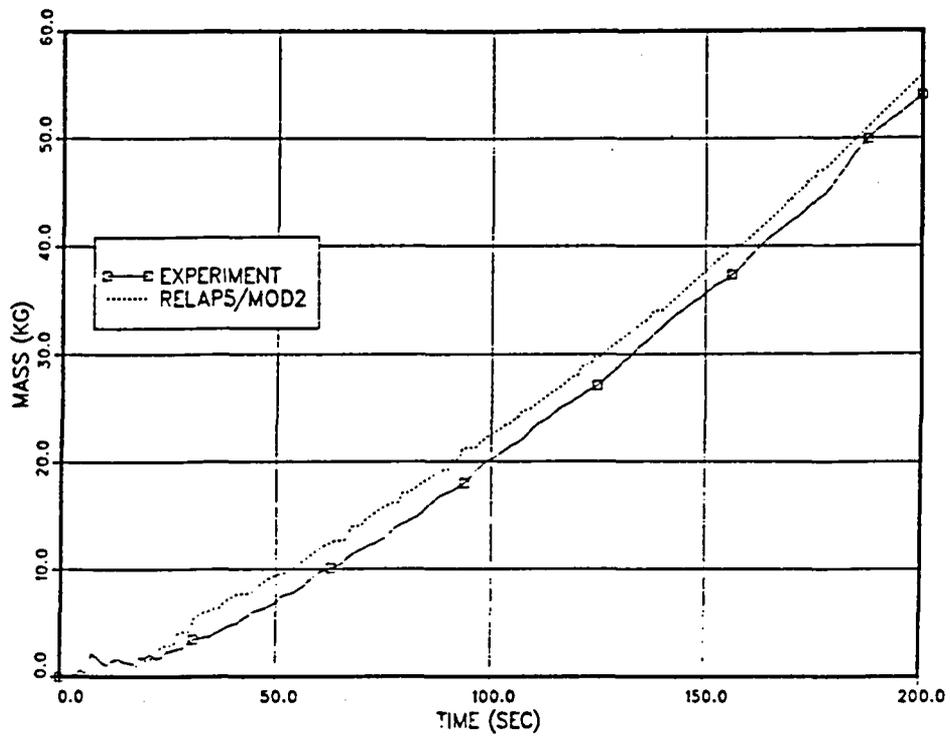


Figure 4.35. EXP 4120; Total mass carry-over.

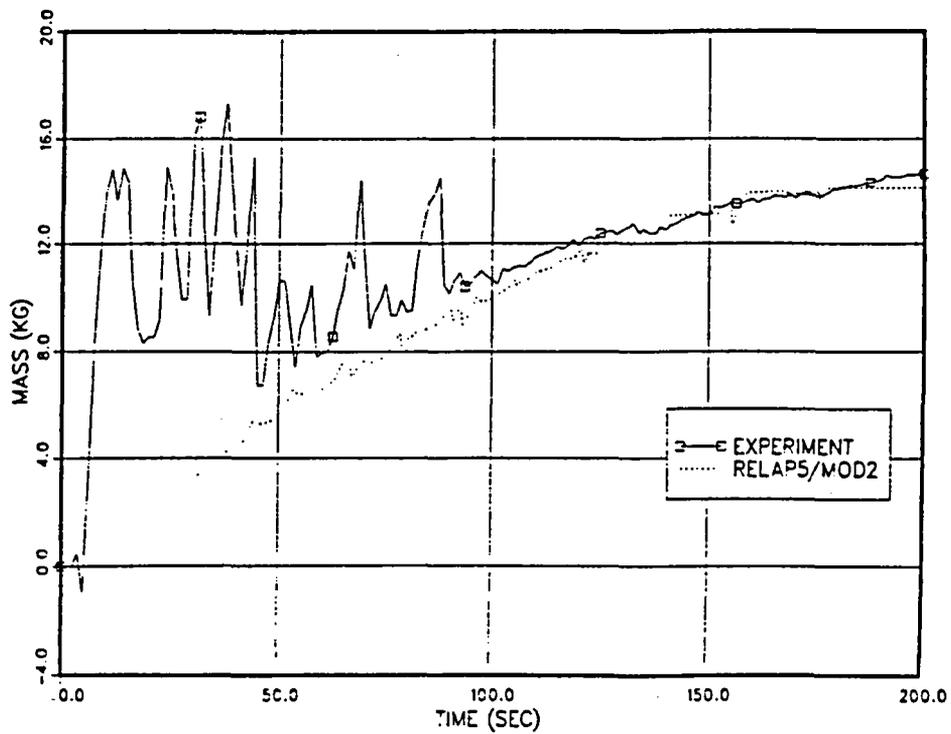


Figure 4.36. EXP 4120; Mass in the bundle.

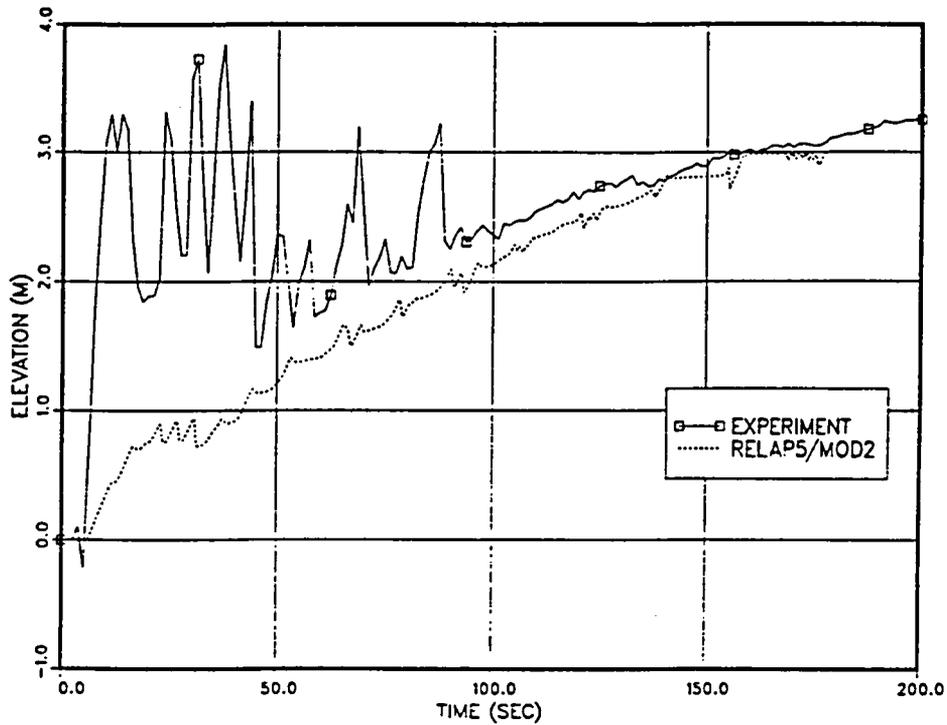


Figure 4.37. EXP 4120; Collapsed liquid level.

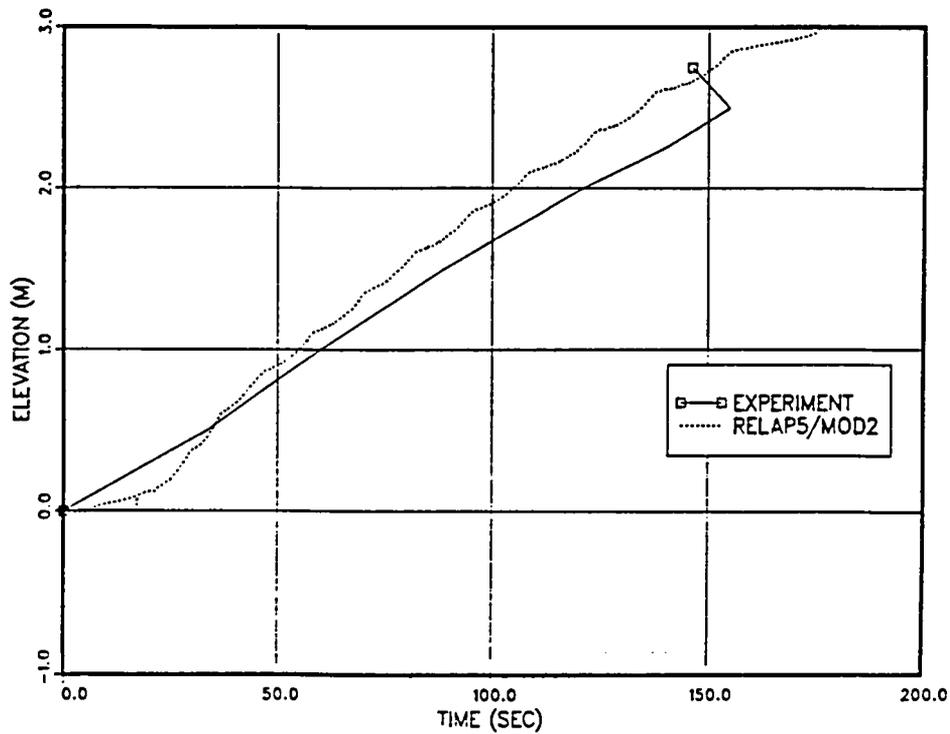


Figure 4.38. EXP 4120; Quench front position.

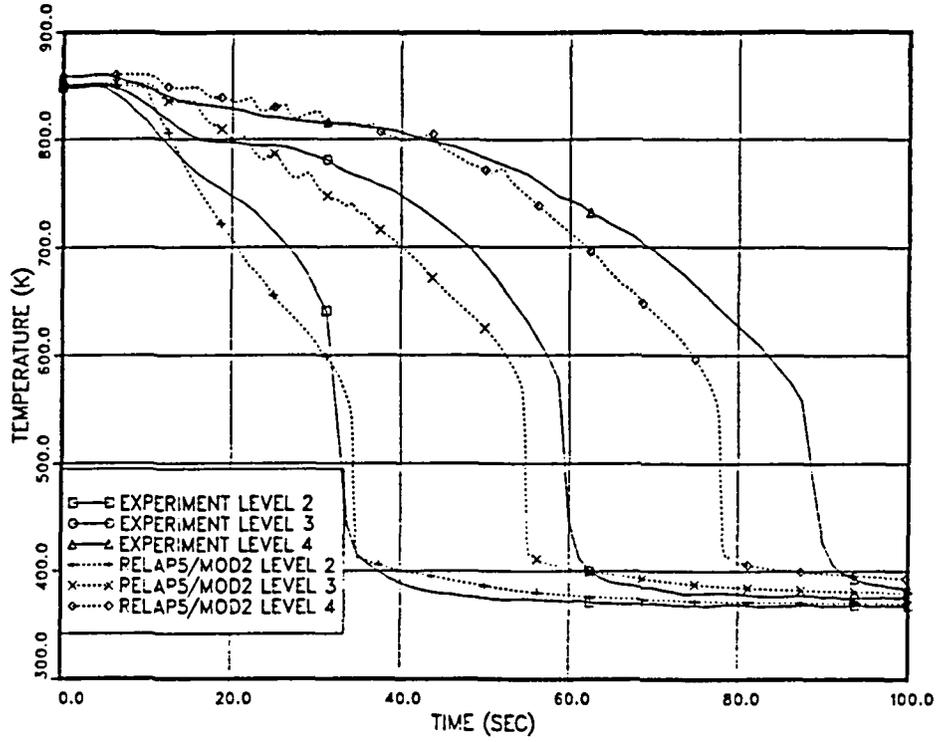


Figure 4.39. EXP 4120; Wall temperatures at level 2, 3, 4.

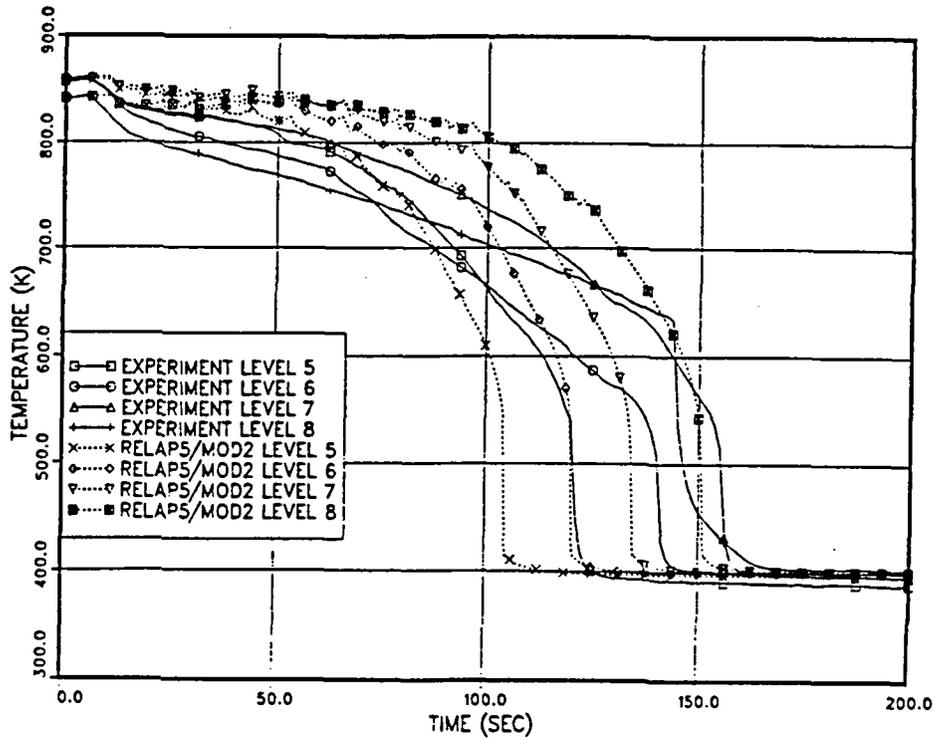


Figure 4.40. EXP 4120; Wall temperatures at level 5, 6, 7, 8.

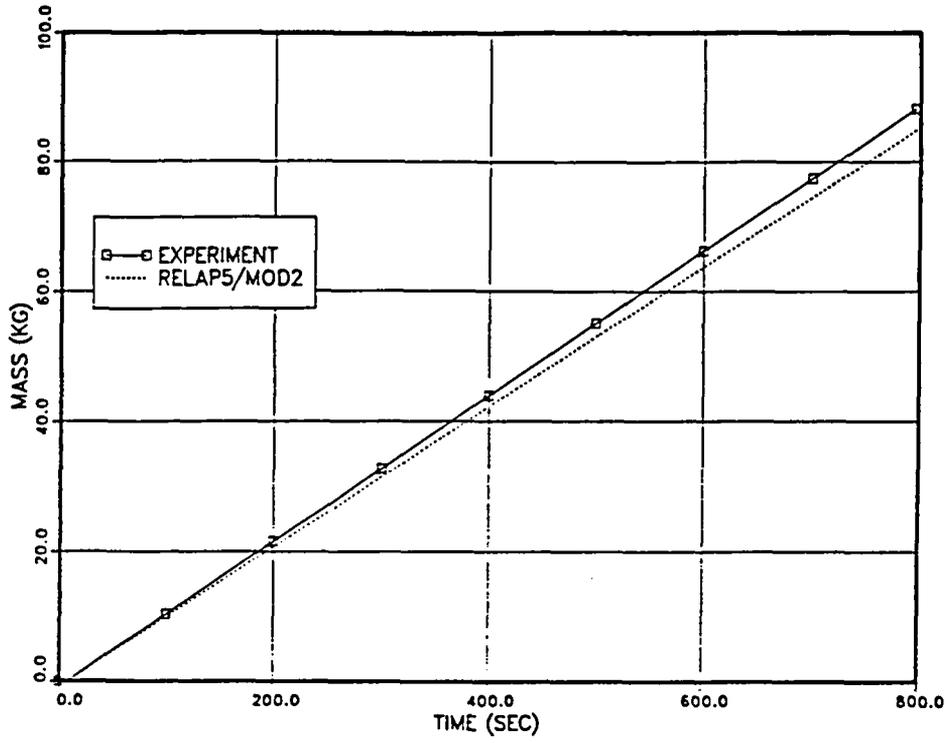


Figure 4.41. EXP 4138; Mass injected.

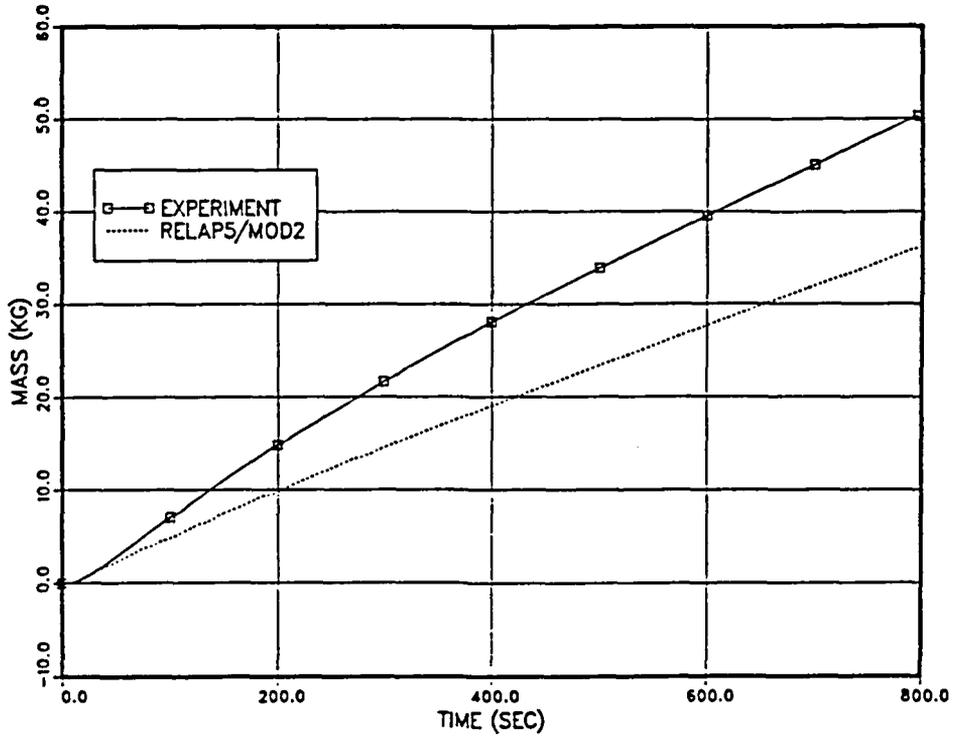


Figure 4.42. EXP 4138; Mass steam out.

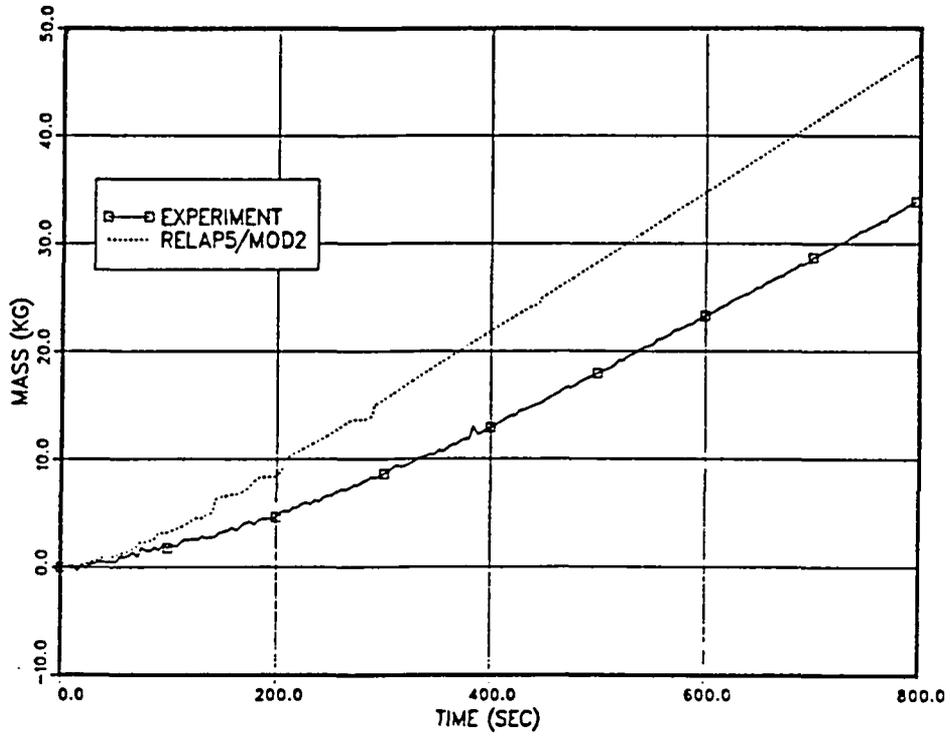


Figure 4.43. EXP 4138; Total mass carry-over.

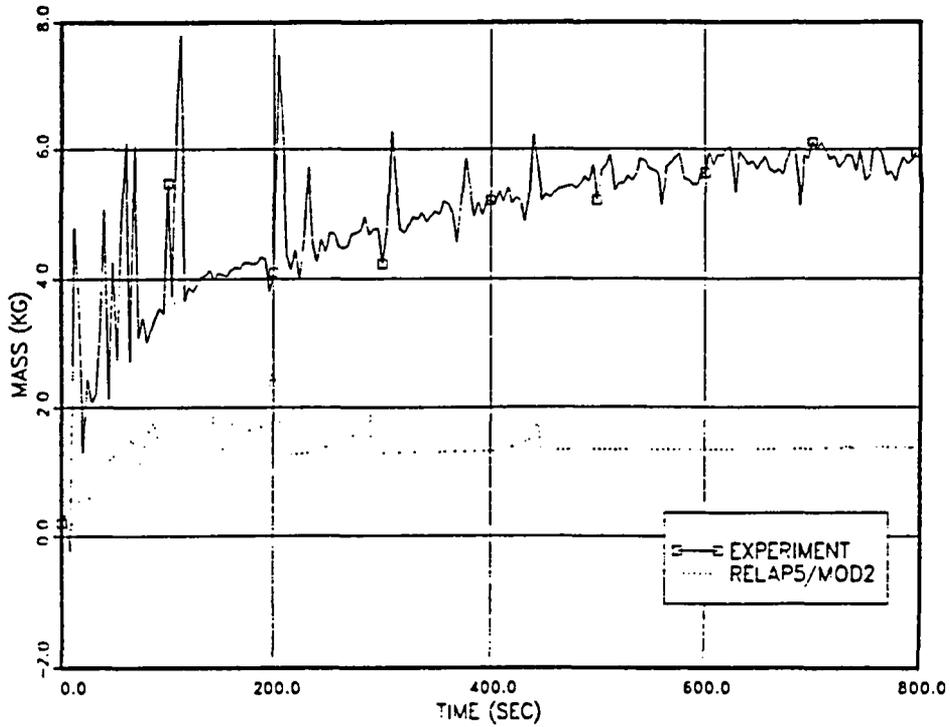


Figure 4.44. EXP 4138; Mass in the bundle.

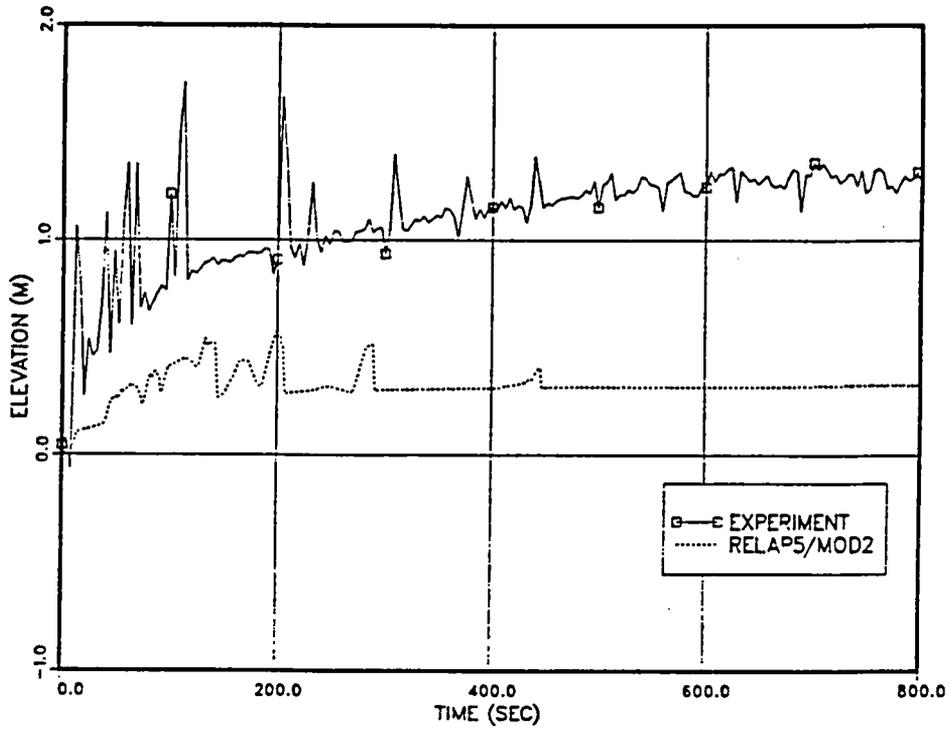


Figure 4.45. EXP 4138; Collapsed liquid level.

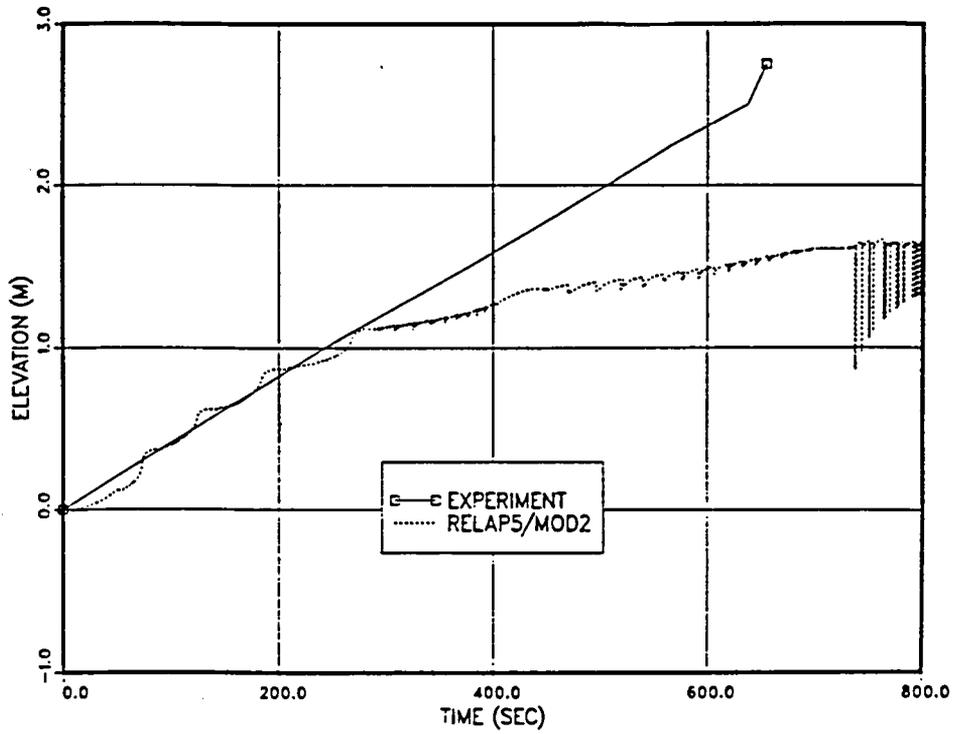


Figure 4.46. EXP 4138; Quench front position.

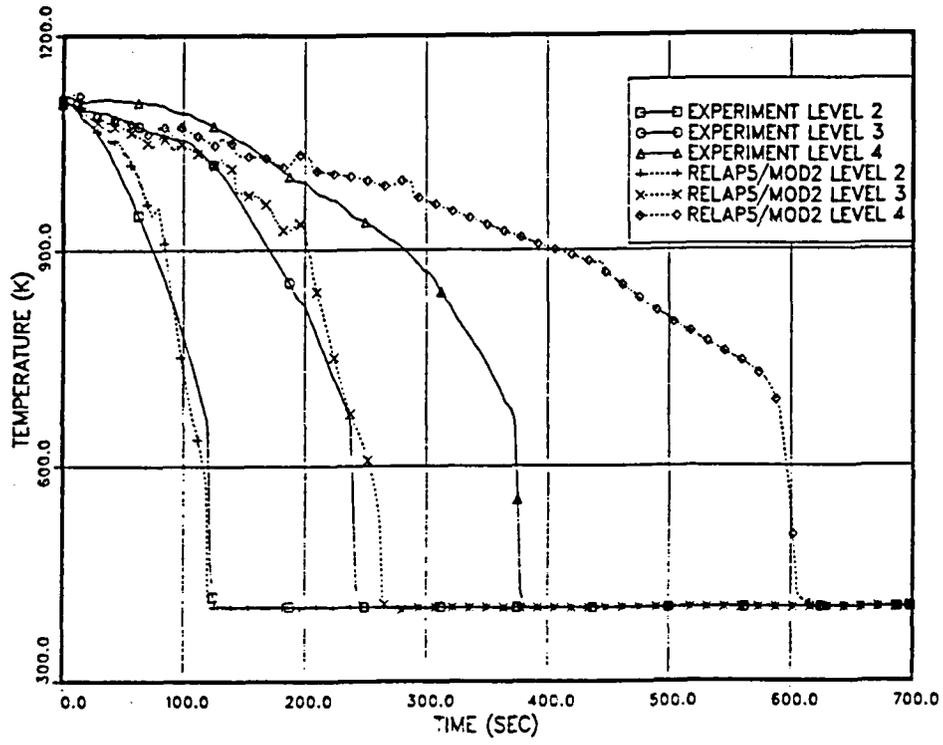


Figure 4.47. EXP 4138; Wall temperatures at level 2, 3, 4.

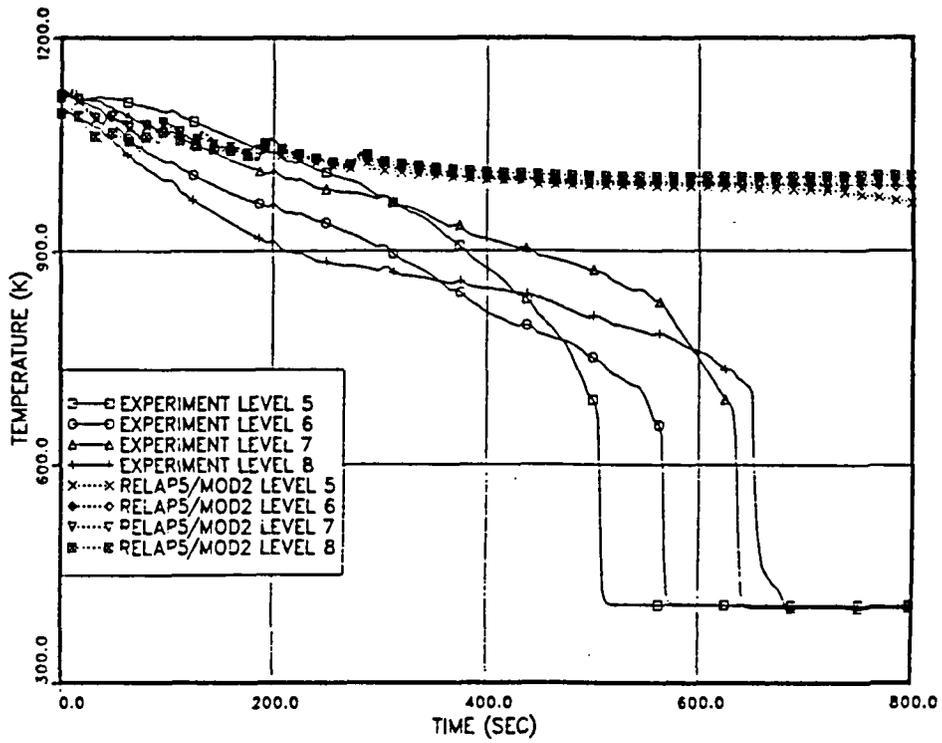


Figure 4.48. EXP 4138; Wall temperatures at level 5, 6, 7, 8.

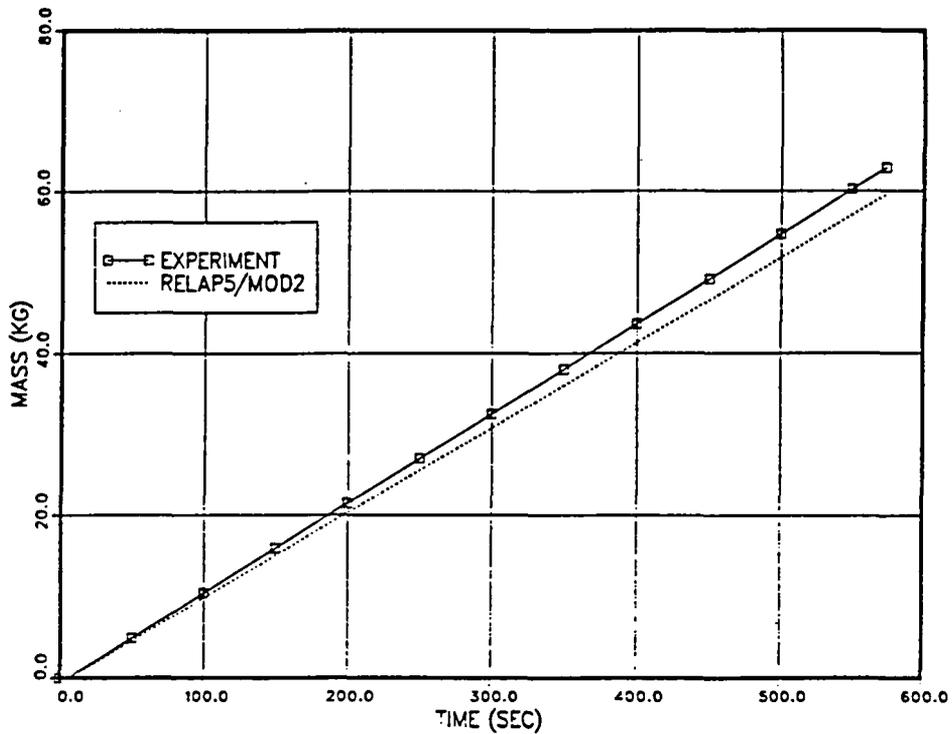


Figure 4.49. EXP 4149; Mass injected.

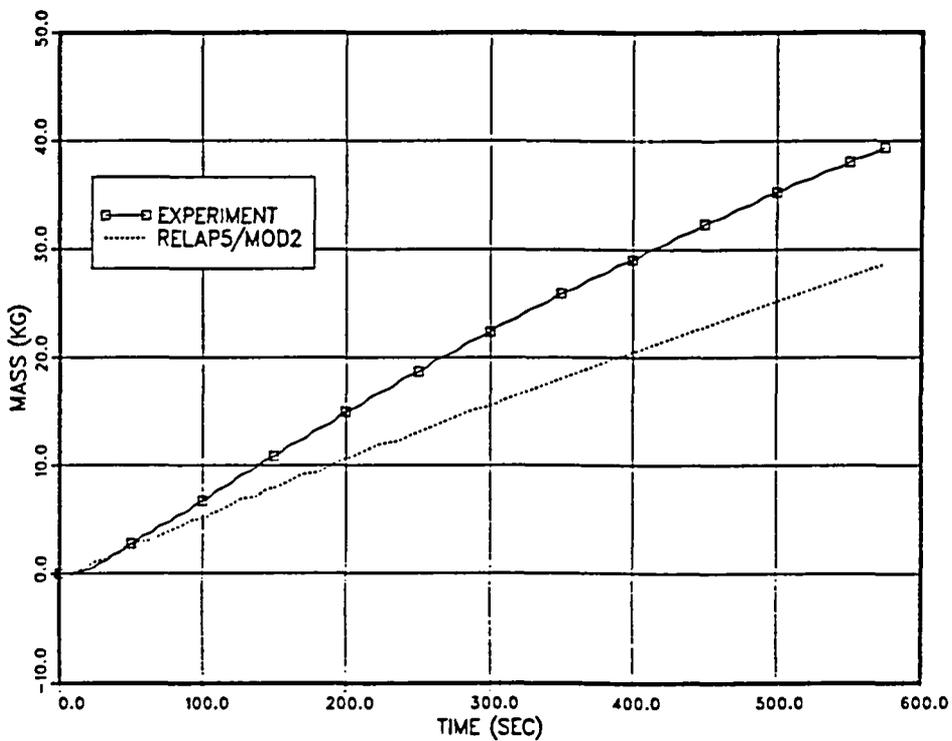


Figure 4.50. EXP 4149; Mass steam out.

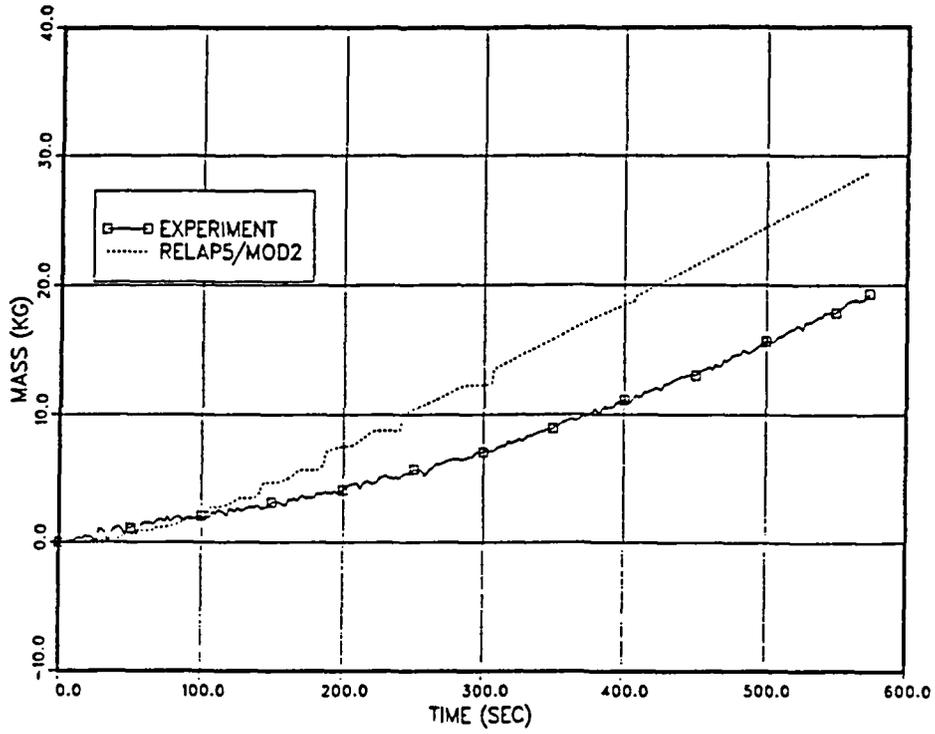


Figure 4.51. EXP 4149; Total mass carry-over.

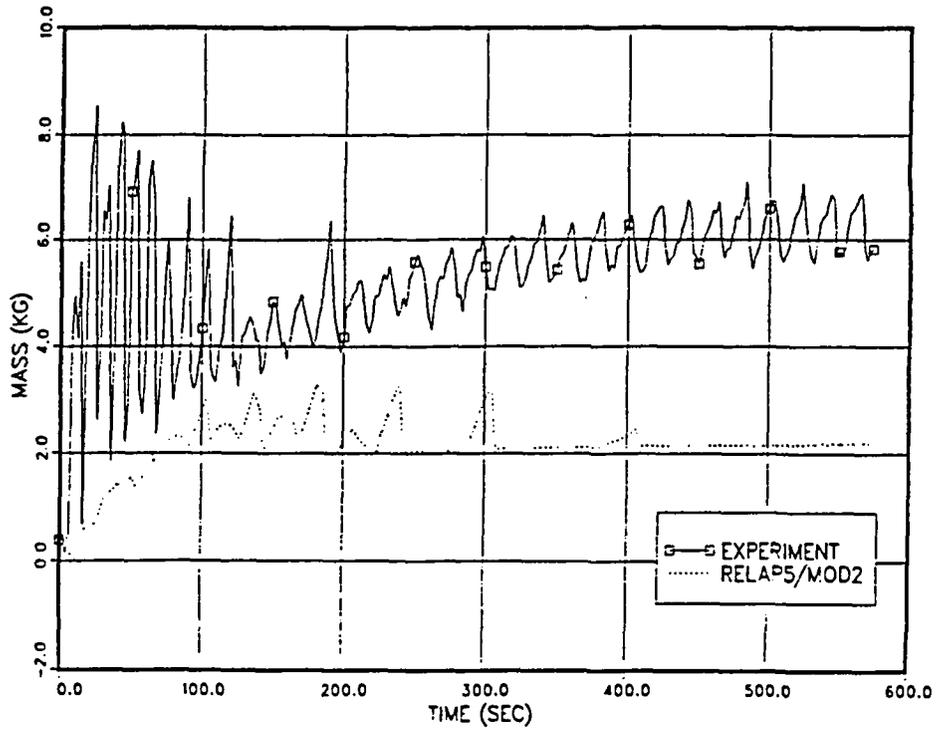


Figure 4.52. EXP 4149; Mass in the bundle.

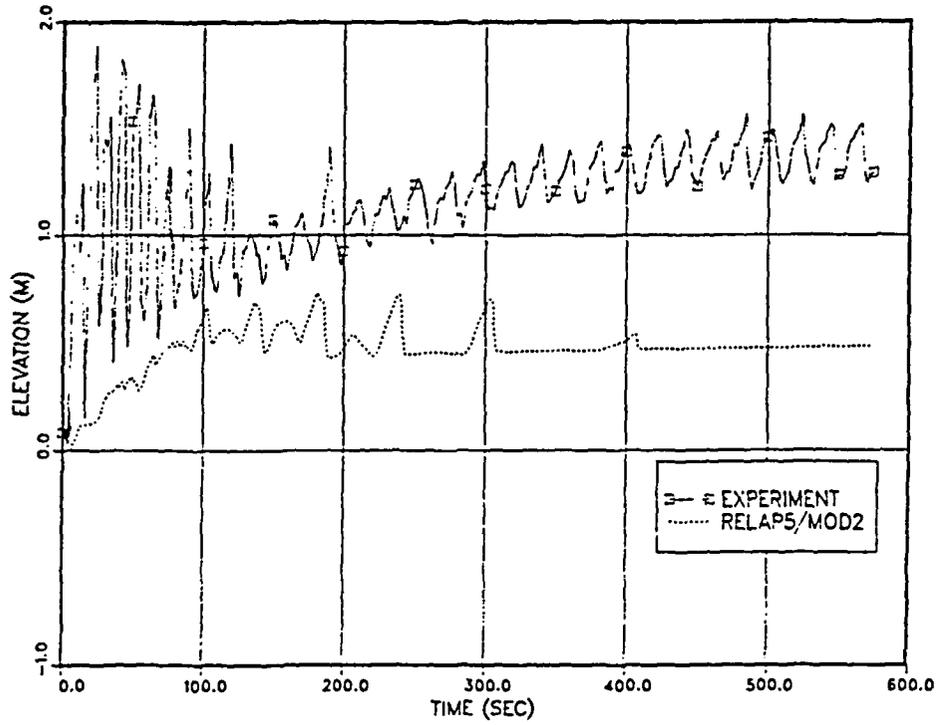


Figure 4.53. EXP 4149; Collapsed liquid level.

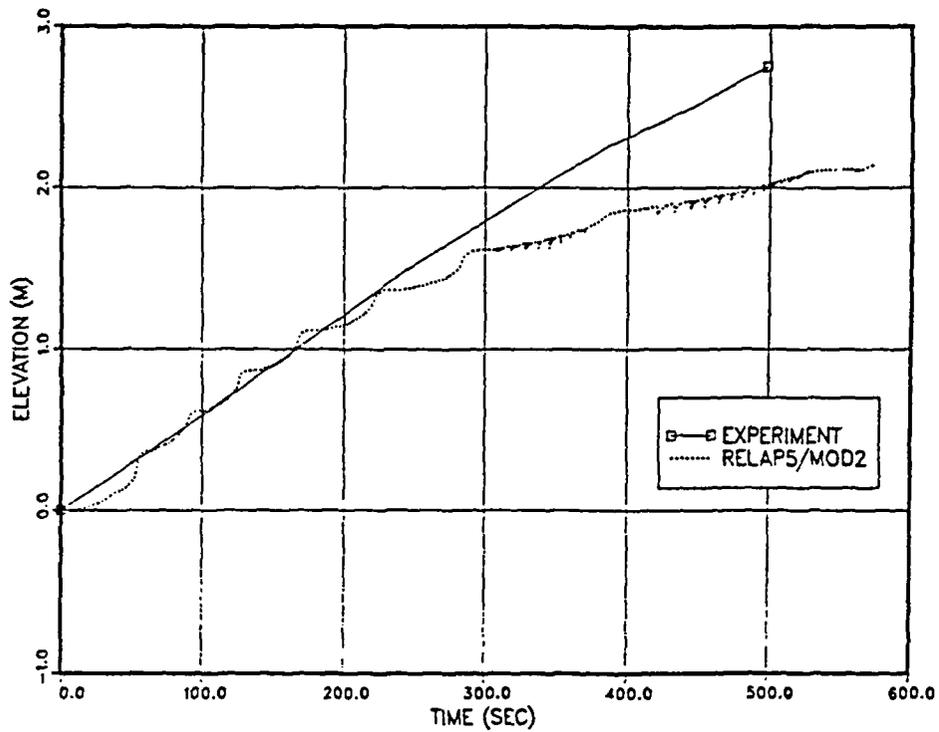


Figure 4.54. EXP 4149; Quench front position.

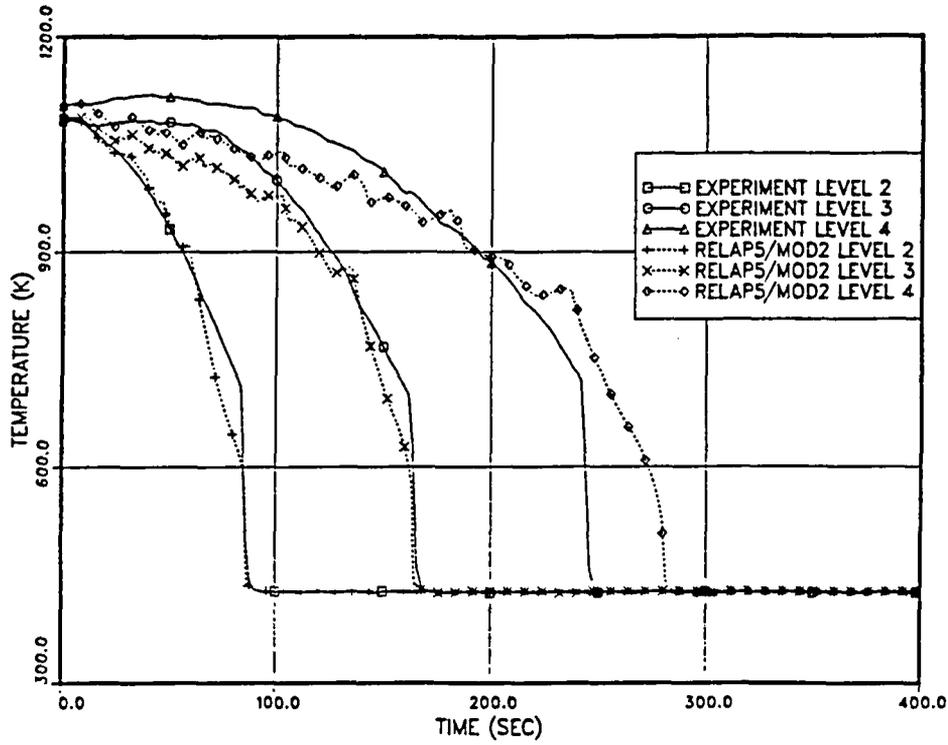


Figure 4.55. EXP 4149; Wall temperatures at level 2, 3, 4.

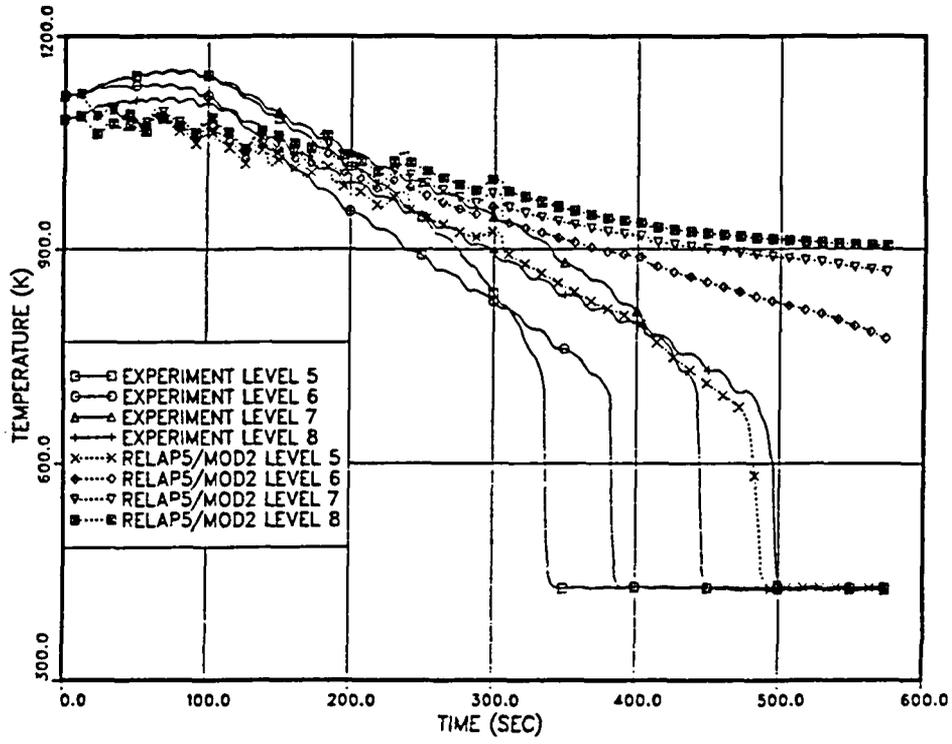


Figure 4.56. EXP 4149; Wall temperatures at level 5, 6, 7, 8.

EXPERIMENTAL RESULTS

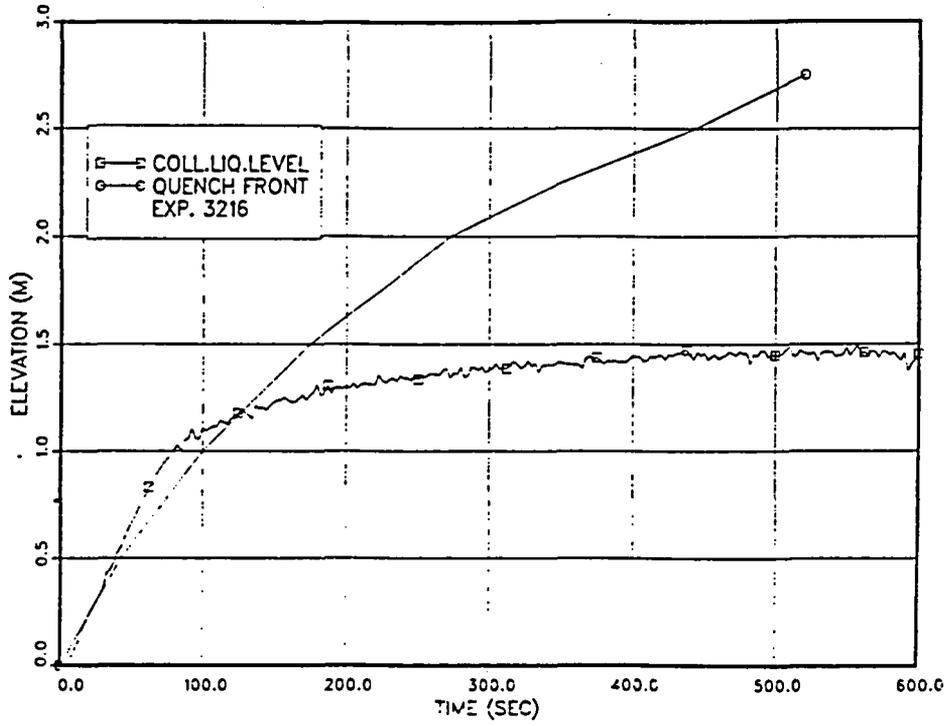


Figure 4.57. EXP 3216; Experimental quench front and collapsed liquid level.

RELAP5/MOD2 RESULTS

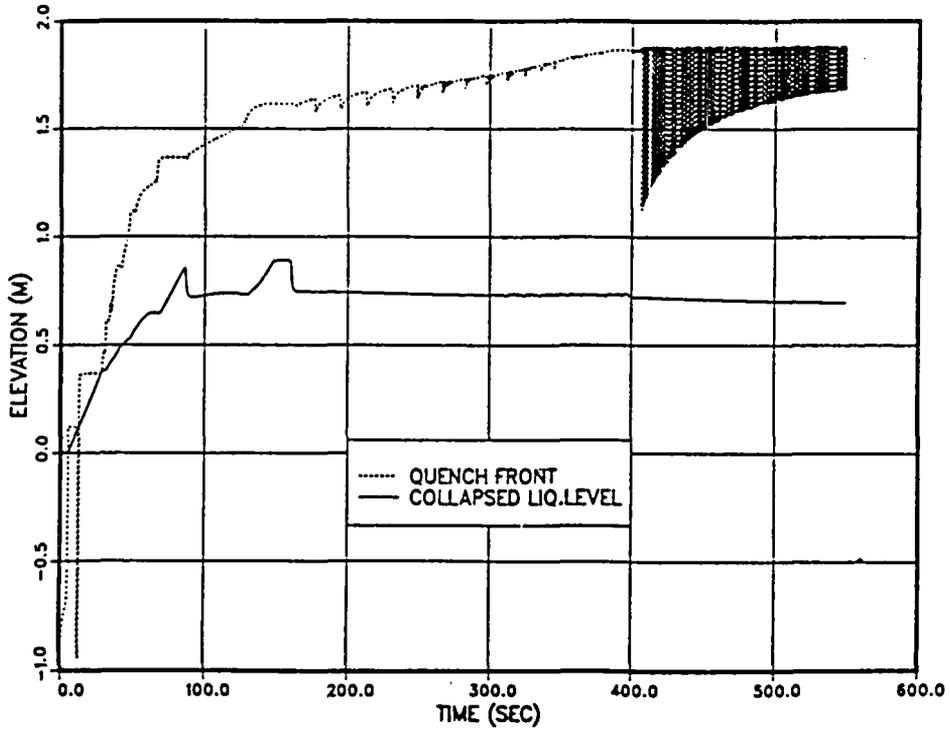


Figure 4.58. EXP 3216; Calculated quench front and collapsed liquid level.

EXPERIMENTAL RESULTS

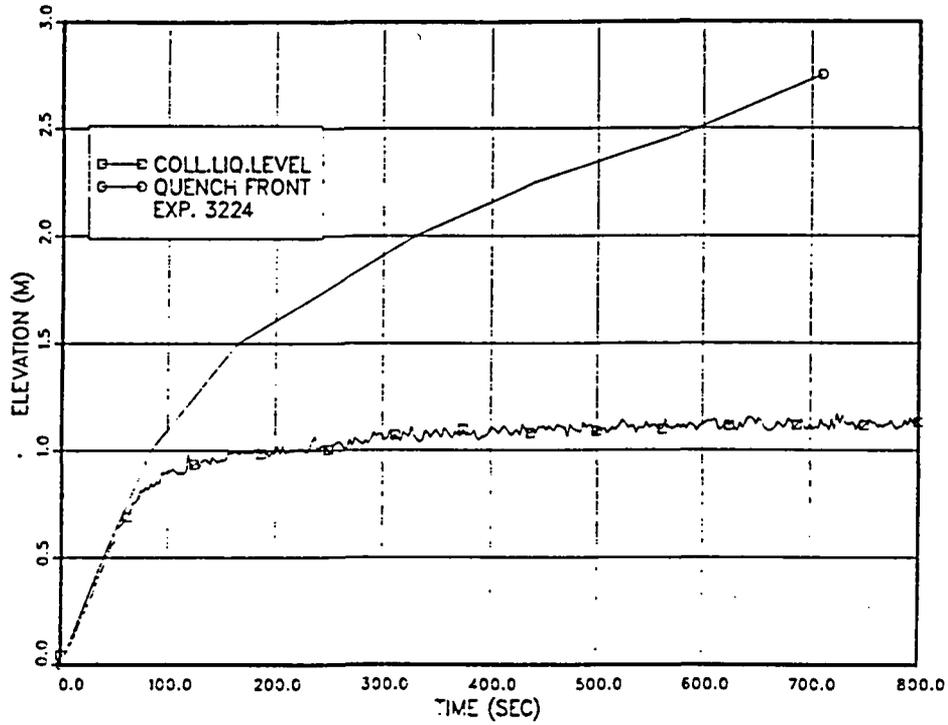


Figure 4.59. EXP 3224; Experimental quench front and collapsed liquid level.

RELAP5/MOD2 RESULTS

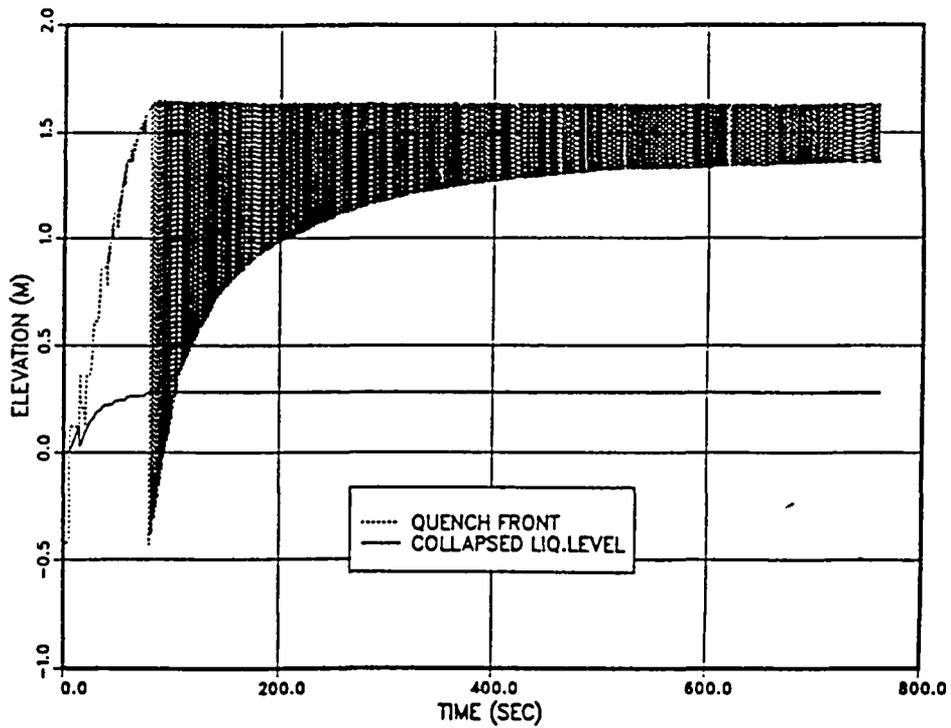


Figure 4.60. EXP 3224; Calculated quench front and collapsed liquid level.

EXPERIMENTAL RESULTS

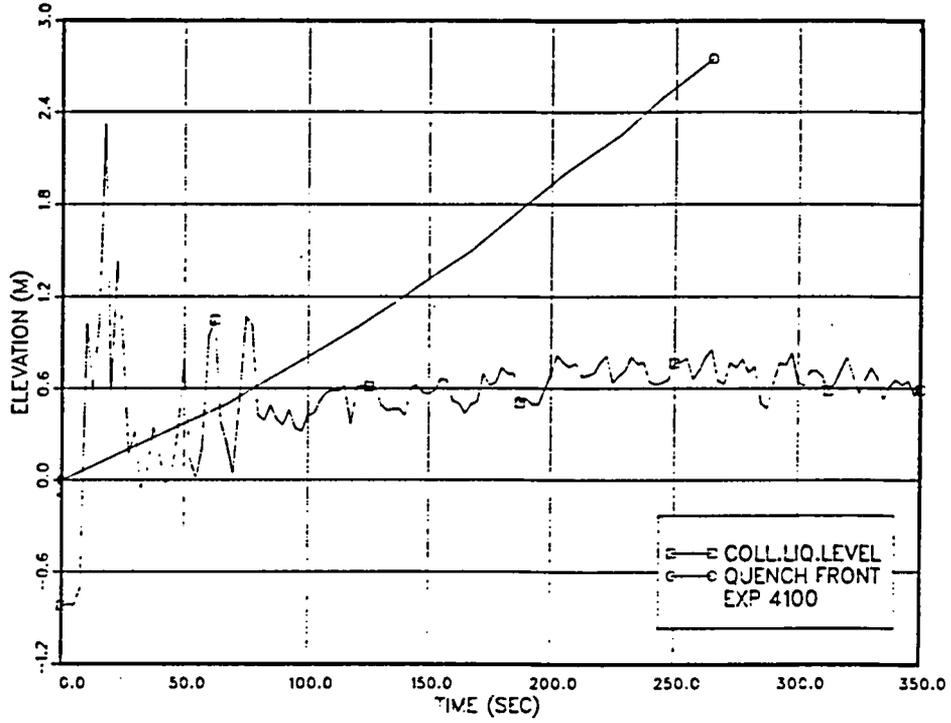


Figure 4.61. EXP 4100; Experimental quench front and collapsed liquid level.

RELAP5/MOD2 RESULTS

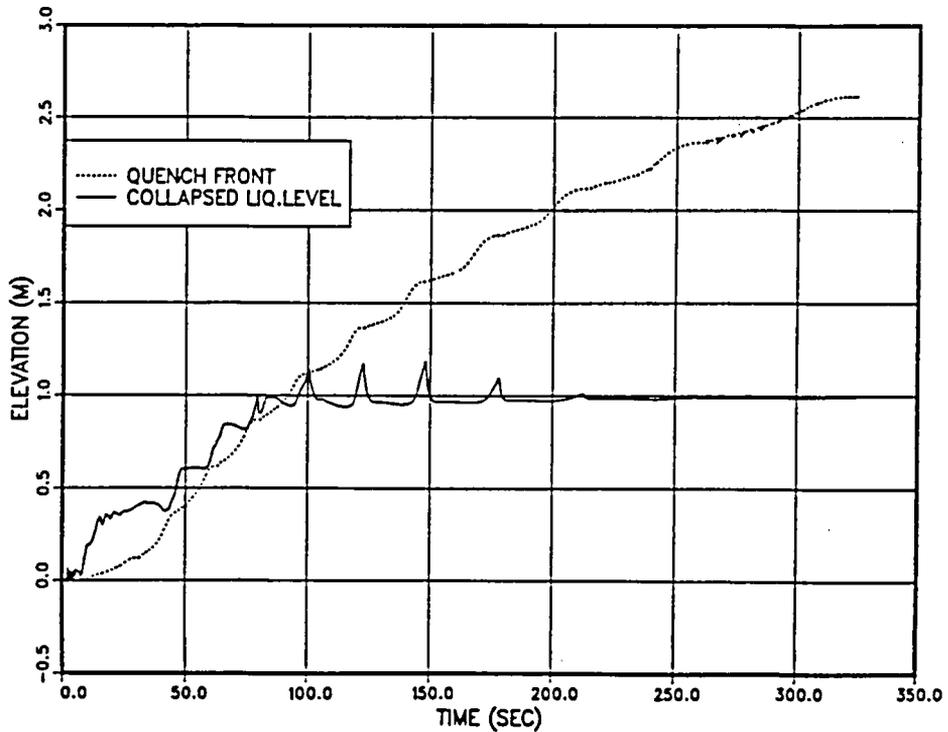


Figure 4.62. EXP 4100; Calculated quench front and collapsed liquid level.

EXPERIMENTAL RESULTS

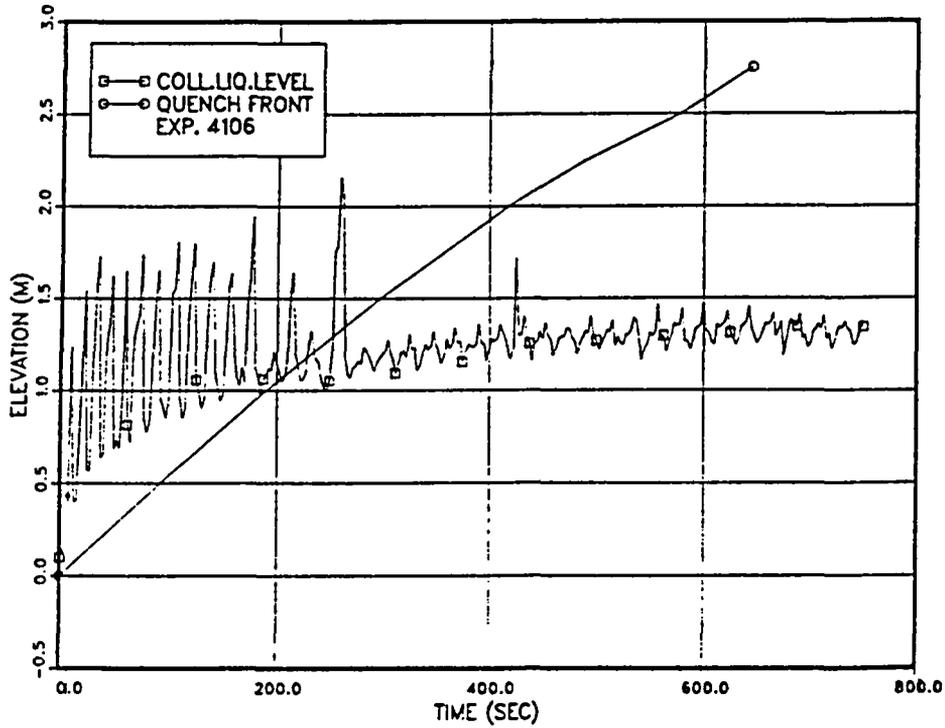


Figure 4.63. EXP 4106; Experimental quench front and collapsed liquid level.

RELAP5/MOD2 RESULTS

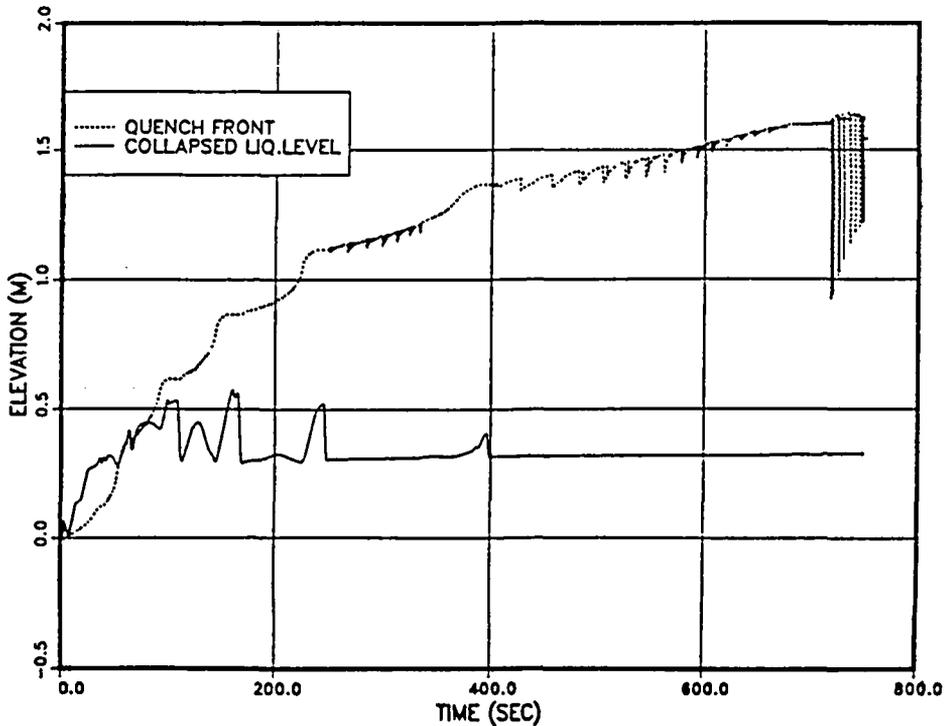


Figure 4.64. EXP 4106; Calculated quench front and collapsed liquid level.

EXPERIMENTAL RESULTS

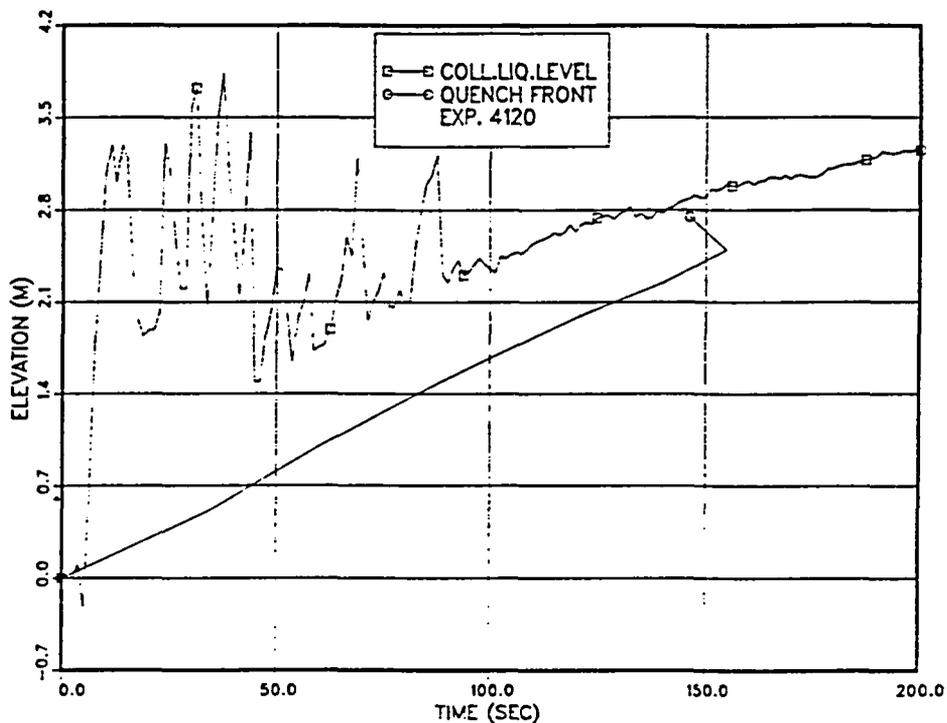


Figure 4.65. EXP 4120; Experimental quench front and collapsed liquid level.

RELAPS/MOD2 RESULTS

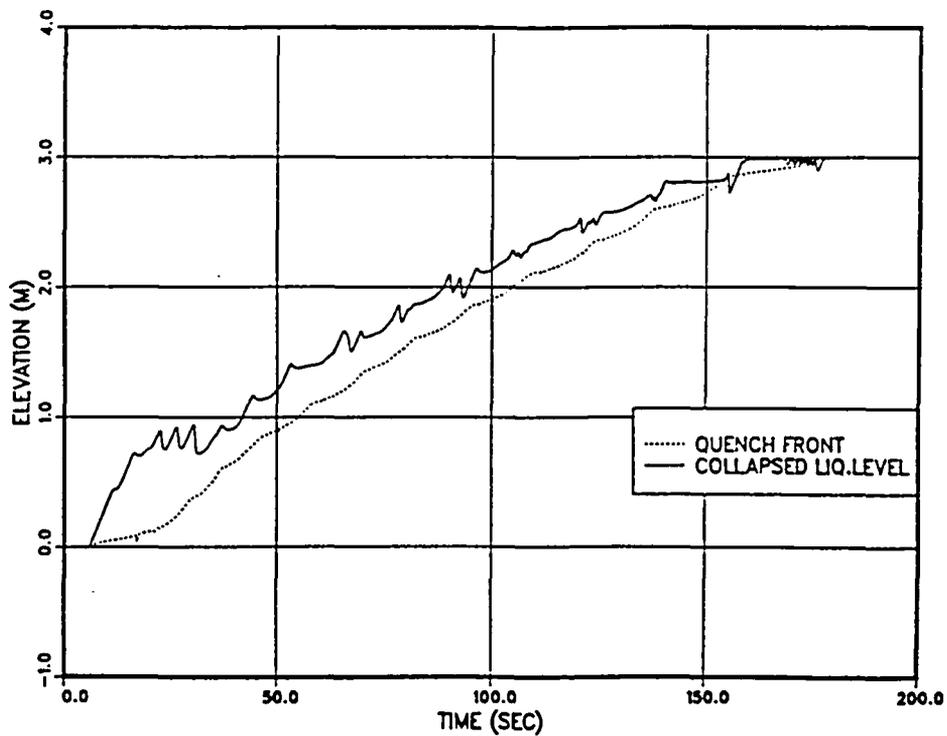


Figure 4.66. EXP 4120; Calculated quench front and collapsed liquid level.

EXPERIMENTAL RESULTS

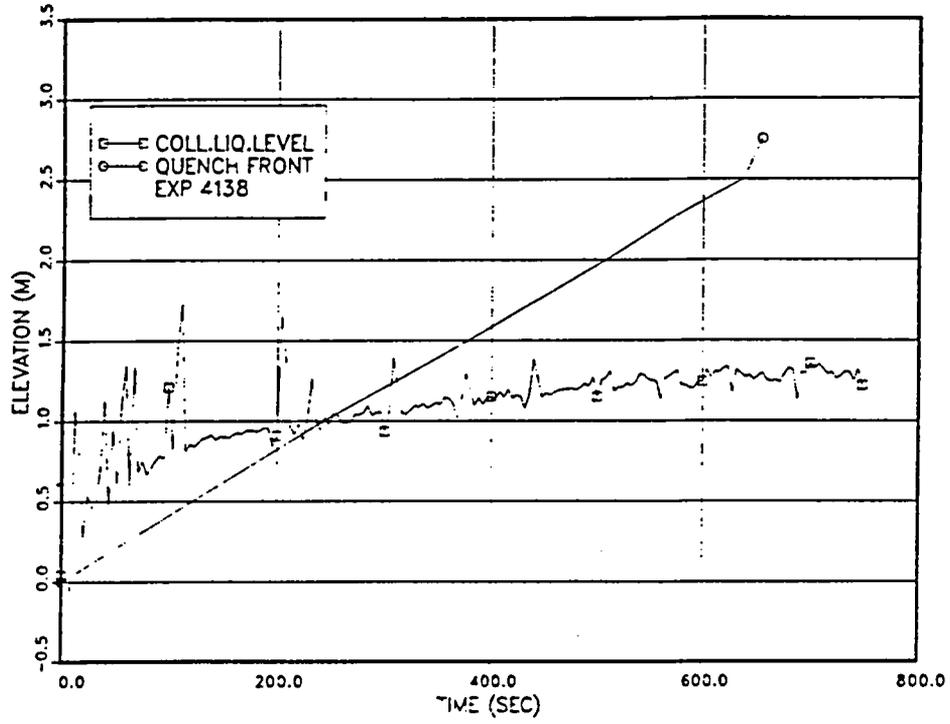


Figure 4.67. EXP 4138; Experimental quench front and collapsed liquid level.

RELAPS/MOD2 RESULTS

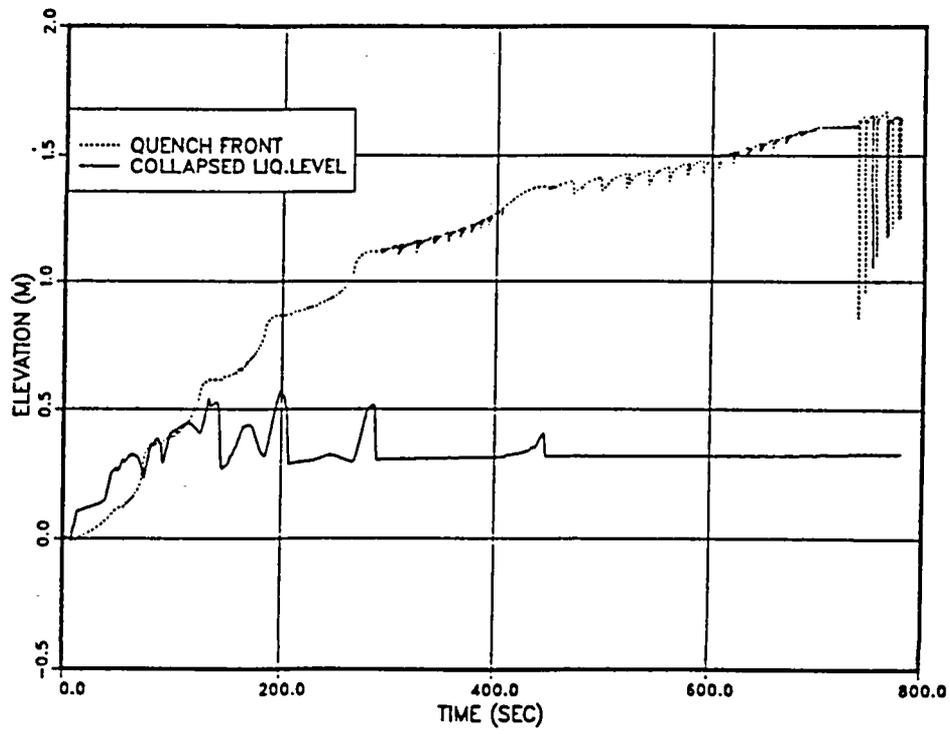


Figure 4.68. EXP 4138; Calculated quench front and collapsed liquid level.

EXPERIMENTAL RESULTS

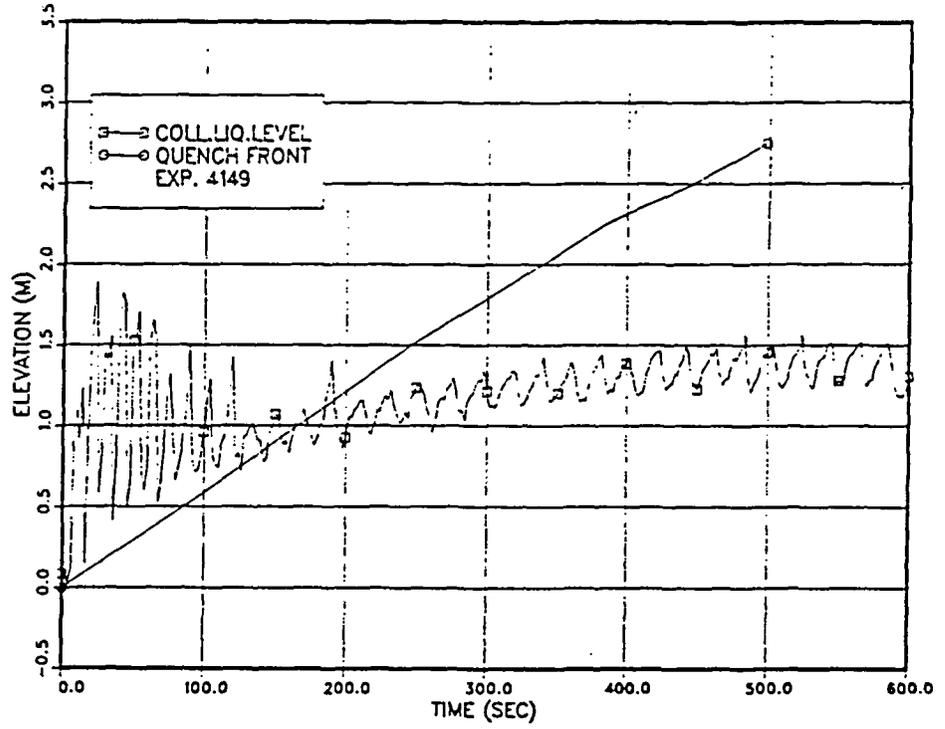


Figure 4.69. EXP 4149; Experimental quench front and collapsed liquid level.

RELAP5/MOD2 RESULTS

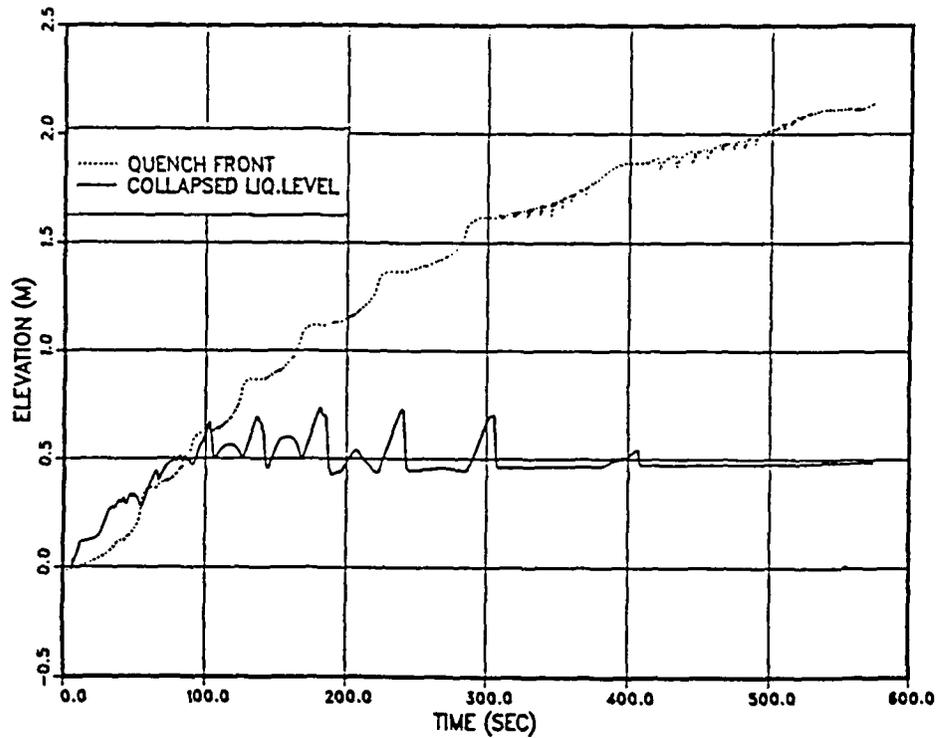


Figure 4.70. EXP 4149; Calculated quench front and collapsed liquid level.

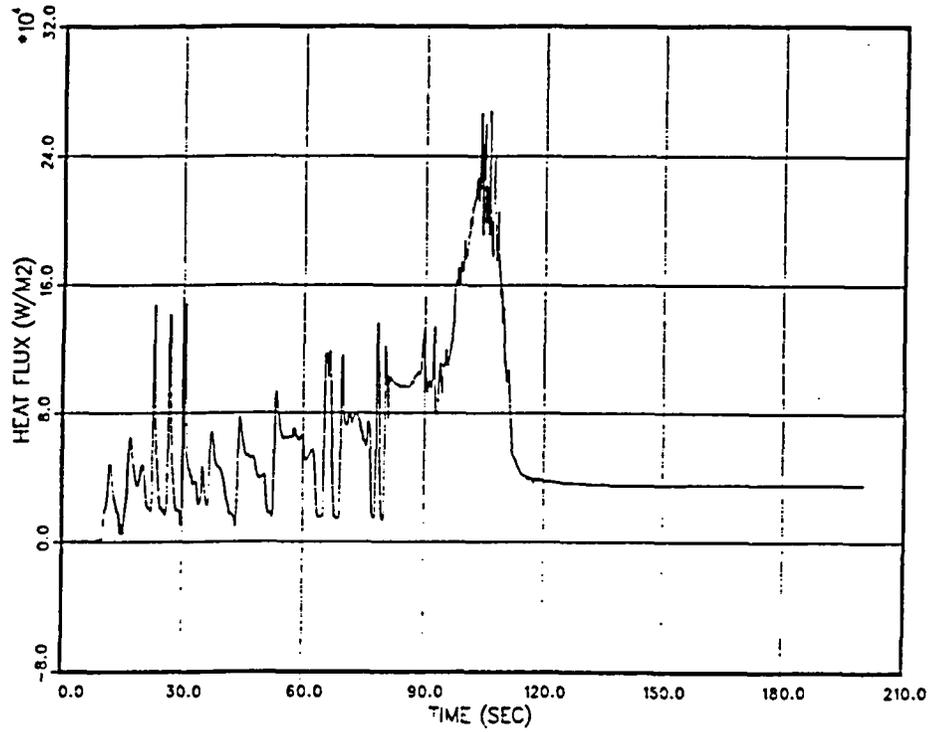


Figure 4.71. EXP 4120; Calculated heat flux at level 5.

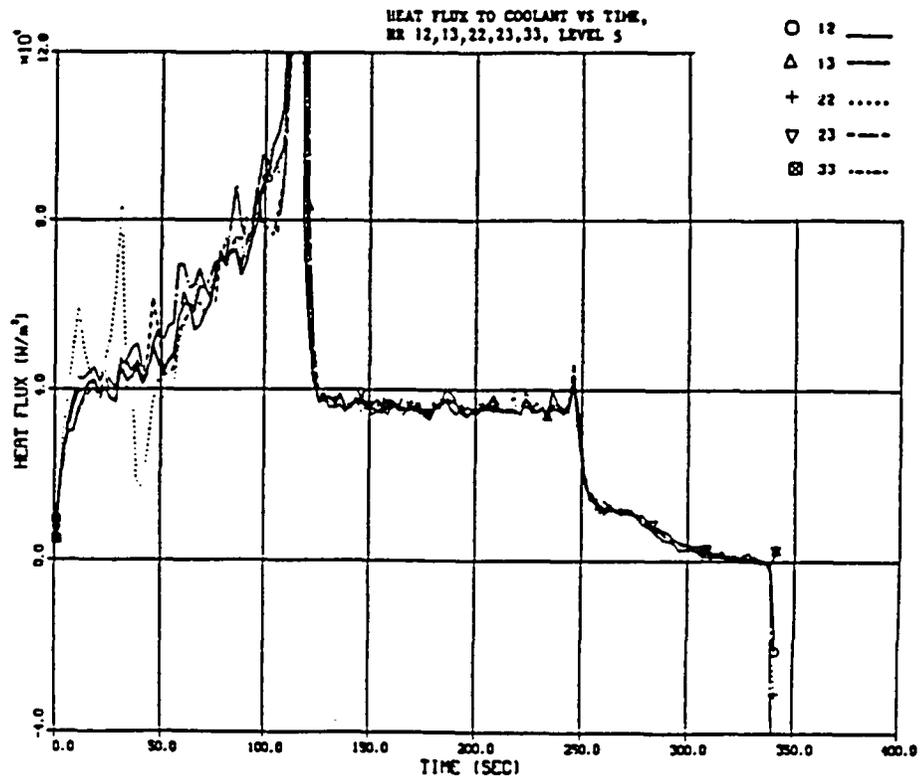


Figure 4.72. EXP 4120; Experimental heat flux at level 5.

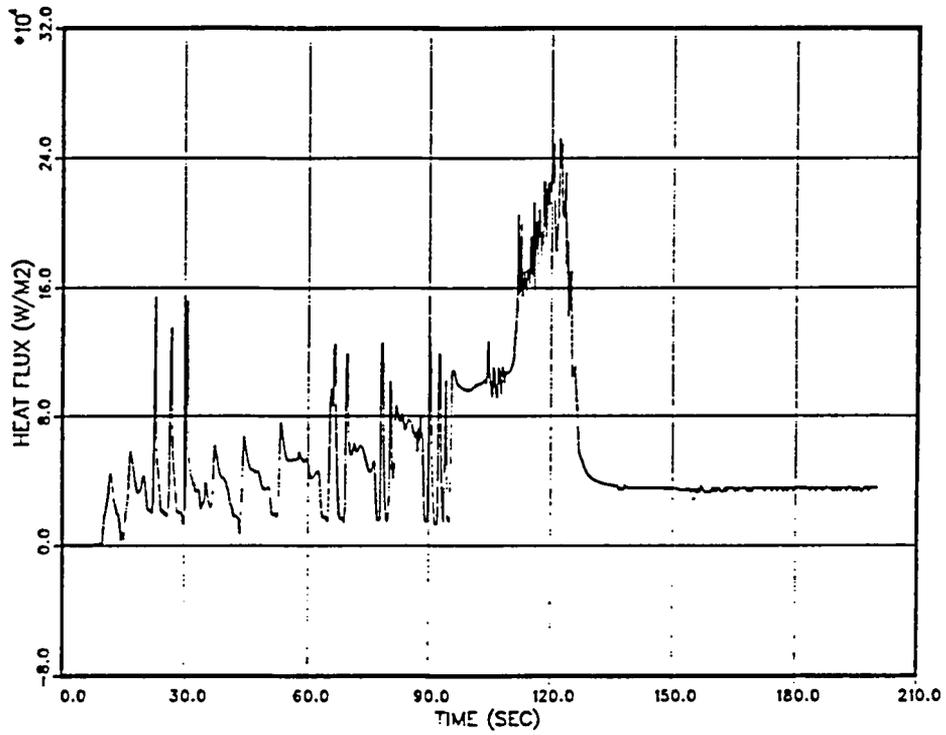


Figure 4.73. EXP 4120; Calculated heat flux at level 6.

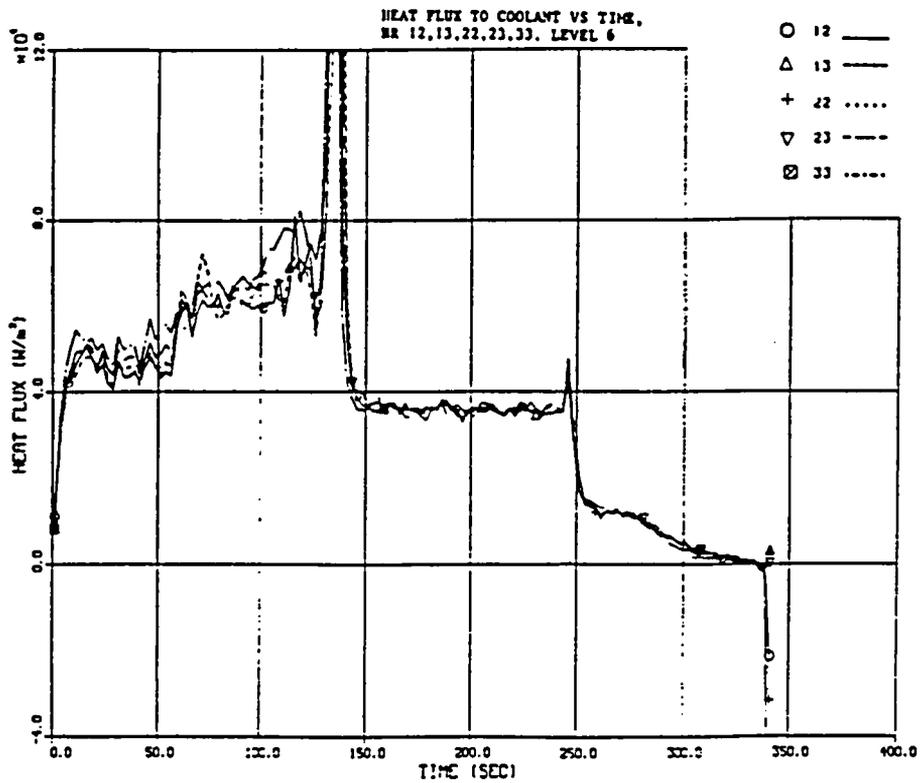


Figure 4.74. EXP 4120; Experimental heat flux at level 6.

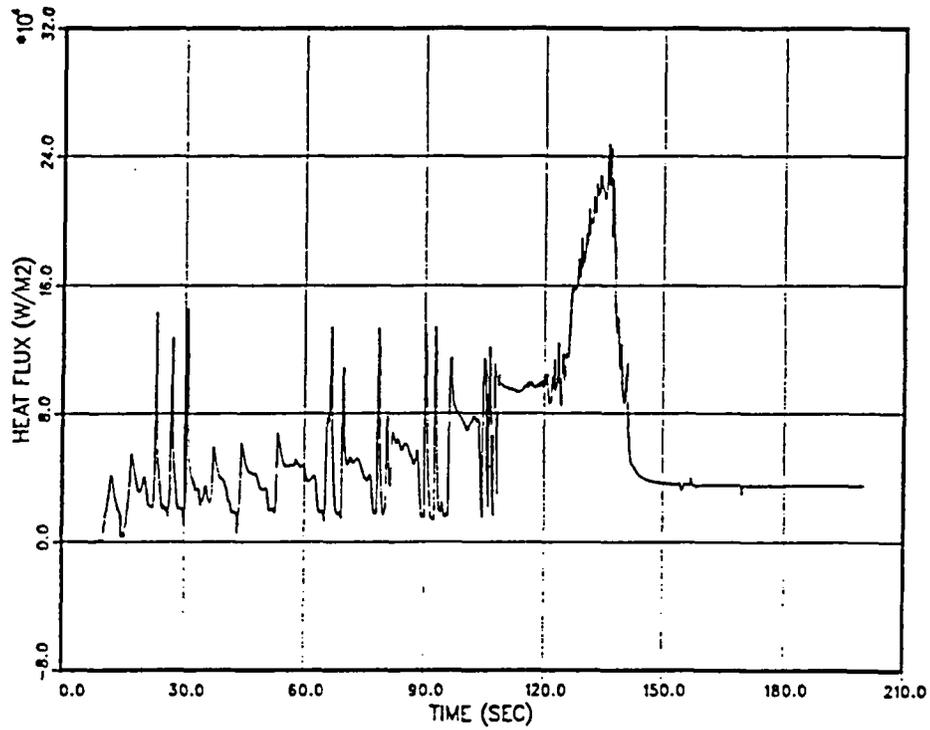


Figure 4.75. EXP 4120; Calculated heat flux at level 7.

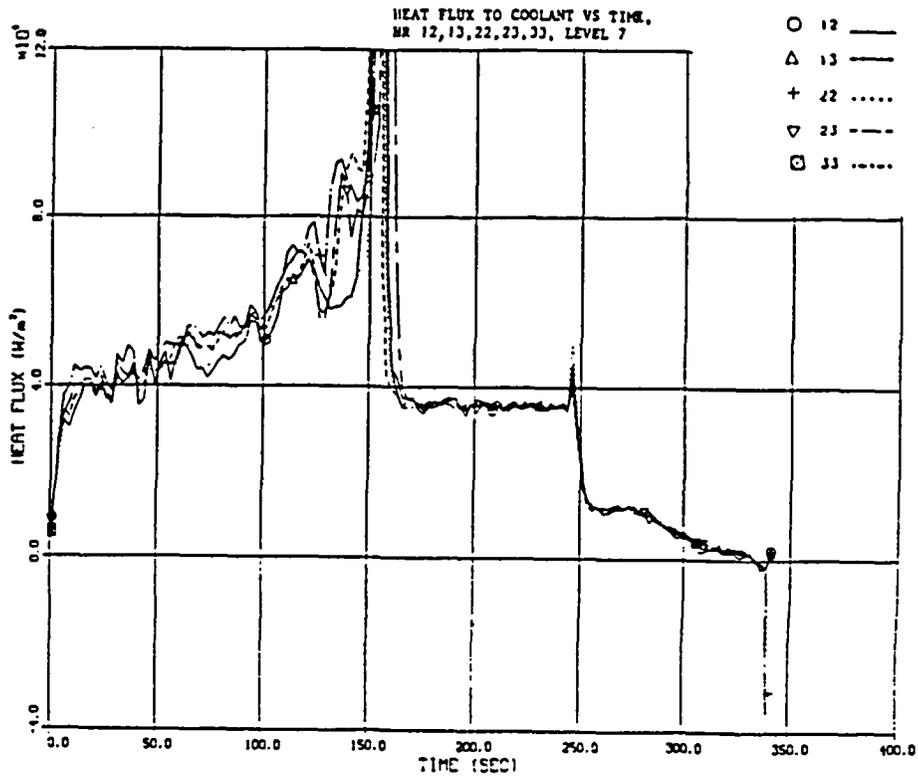


Figure 4.76. EXP 4120; Experimental heat flux at level 7.

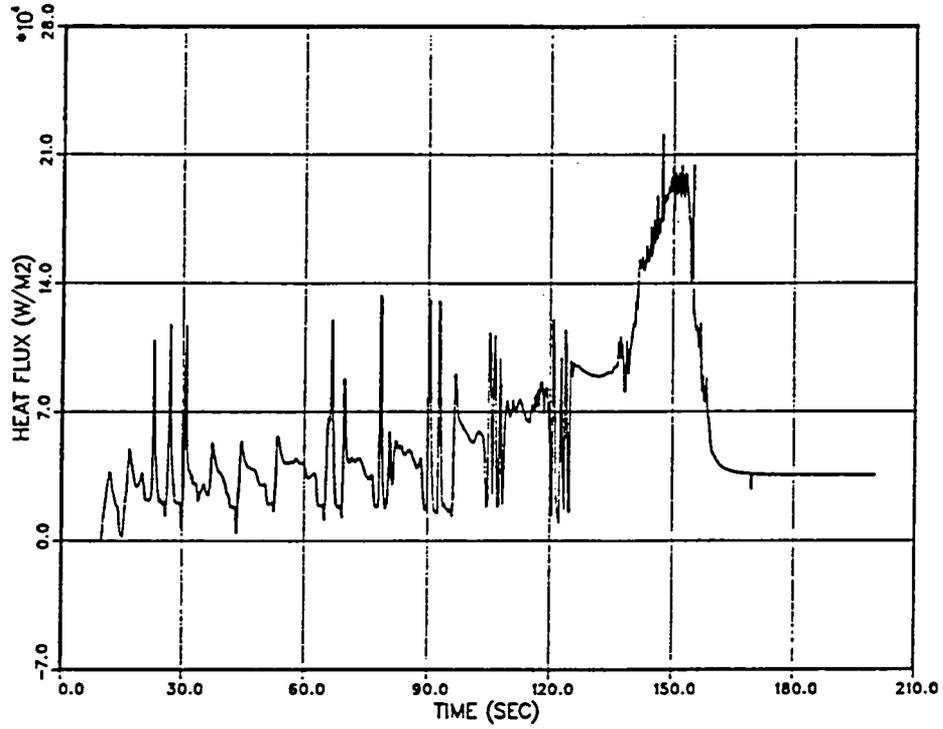


Figure 4.77. EXP 4120; Calculated heat flux at level 8.

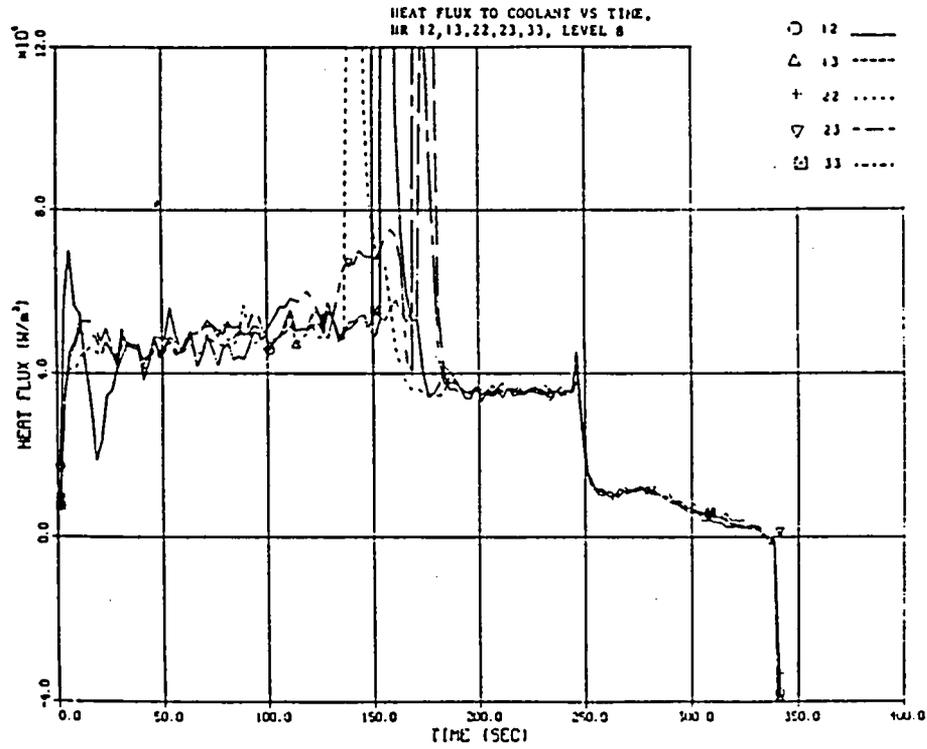


Figure 4.78. EXP 4120; Experimental heat flux at level 8.

5. RUN STATISTICS

The number of system seconds and the CPU time used for the four sensitivity analyses as presented in section 3.1. are given in Table 5.1. The numbers are based on 100 seconds process time. The analyses are performed on the Cyber 855 mainframe computer of the Technical Computing Center (ENR) at Petten, the Netherlands.

Table 5.1. Run statistics.

	Length of the hydrodynamic nodes	Axial fine mesh intervals	CPU (s)	Process time (s)
Run 1; Exp. 100	.125 m	16	2429	100
Run 2; Exp. 4100	.125 m	32	2554	100
Run 3; Exp. 4100	. 25 m	32	909	100
Run 4; Exp. 4100	. 50 m	32	593	100

6. CONCLUSIONS

The conclusions concerning the RELAP5/MOD2 analyses of some selected reflood experiments can be summarized as follows:

- The reflood heat transfer model in RELAP5/MOD2 is only valid for high reflood rates. This is the main reason that cladding temperatures are well predicted for high reflood velocities (0.08 m/s) while a poor comparison is obtained for low reflood velocities (0.015 m/s). Modification of the heat transfer model to include low reflood rates is recommended.
- Entrainment of water in the bundle is strongly overpredicted for all selected cases. For this reason modifications of the interfacial friction correlations for the bubbly and slug flow regime are recommended.
- Refinement of the axial nodalization (axial nodes smaller than recommended in the RELAP5/MOD2 users guidelines) does not improve the calculational results.

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Appendix A. RELAP5/MOD2 input deck.

= REFLOOD EXP 3216

*

100 NEW STDY-ST

101 RUN

*

*TIME STEPS

*

*	END	MIN	MAX	CTRL	MINED	MAJED	REST
201	0.5	.5E-4	.01	202	25	1000	1250

*

*****20800001 TREWET 3101

*****20800002 ZTRWT 3101

*

*MINOR EDITS

*

301 P 310150000

*****302 ZTRWT 3101

303 HTTEMP 310100505

304 HTTEMP 310100705

305 HTTEMP 310100905

306 HTTEMP 310101105

307 HTTEMP 310101205

308 HTTEMP 310101305

309 HTTEMP 310101405

*

*TRIPS

*

501	TIME	0	GT	NULL	0	1000. N	*END
510	TIME	0	GT	NULL	0	10.0 L	*POWER
520	TIME	0,	GT	NULL	0	10.0 L	*FILL FLOW
530	TIME	0	GT	NULL	0	.0 L	*REFLOOD
600	501						

*

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* * * * *
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* * * * *
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*

* VOLUMES

*

01100000	INLET	TMDPVOL					
01100101	1000000.	100.	.0	.0	90.	100.	
01100102	4.0E-5	0.0	00				
01100200	3						
01100201	0.	200000.	313.				

*

03100000	HEATER	PIPE						
03100001	15							
03100101	.004785	15						
03100201	.0	1						
03100202	.0	2						
03100203	.004188	3						
03100204	.0	4						
03100205	.004188	5						
03100206	.0	6						
03100207	.004188	7						
03100208	.0	8						
03100209	.004188	9						
03100210	.0	10						
03100211	.004188	11						
03100212	.0	12						
03100213	.004188	13						
03100214	.0	14						
03100301	.125	3						
03100302	.25	14						
03100303	.125	15						
03100601	90.	15						
03100801	4.0E-5	.0118	15					
03100901	.0	.0	1					
03100902	.0	.0	2					
03100903	.0717	.0717	3					
03100904	.0	.0	4					
03100905	.0717	.0717	5					
03100906	.0	.0	6					
03100907	.0717	.0717	7					
03100908	.0	.0	8					
03100909	.0717	.0717	9					
03100910	.0	.0	10					
03100911	.0717	.0717	11					
03100912	.0	.0	12					
03100913	.0717	.0717	13					
03100914	.0	.0	14					
03101001	00	15						
03101101	31000	14						
03101201	3	201309.	313.0	.0	.0	.0		1
03101202	0	200105.	166795.	2529480.	.10	.0		2
03101203	3	200029.	463.	.0	.0	.0		3
03101204	3	200027.	463.	.0	.0	.0		4
03101205	3	200024.	463.	.0	.0	.0		5
03101206	3	200017.	463.	.0	.0	.0		12
03101207	3	200007.	463.	.0	.0	.0		13
03101208	3	200005.	463.	.0	.0	.0		14
03101209	3	200003.	463.	.0	.0	.0		15
03101300	1							
03101301	.0	.0	.0		14			

*

04100000	UPPLEN	SEPARATR				
04100001	3	0				
04100101	.004785	.25	0.	0.	90.	.25
04100102	4.0E-5	.0118	00			
04100200	3	200000.	453.			
04101101	410010000	950000000	.004785	.5	.5	31000
04101201	0.0	0.0	0.0			
04102101	410000000	955000000	.004785	.5	.5	31000
04102201	0.0	0.0	0.0			
04103101	310010000	410000000	.004785	.0	.0	31000
04103201	0.0	0.0	0.0			
*						
09500000	OUTLET	TMDPVOL				
09500101	1000000.	100.	.0	.0	90.	100.
09500102	4.0E-5	0.	00			
09500200	3					
09500201	0.	200000.	453.0			
*						
09550000	OUTLET	TMDPVOL				
09550101	1000000.	100.	.0	.0	90.	100.
09550102	4.0E-5	0.	00			
09550200	3					
09550201	0.	200000.	453.0			
*						
01150000	INLET	TMDPJUN				
01150101	110000000	310000000	.0			
01150200	0	520				
01150201	0.0	.0	.0	.0		
01150202	4.9	.0	.0	.0		
01150203	5.0	.015486	.0	.0		
01150204	805.0	.014356	.0	.0		
*						
*						

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* * * **** * ***** ***** ***
* * * * * * * * * *
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*
13101000 15 5 2 0 0. 530 1 32
13101100 0 1
13101101 1 .0023
13101102 1 .0025
13101103 1 .00446
13101104 1 .00535
13101201 1 1
13101202 2 2
13101203 1 3
13101204 3 4
13101301 0. 1
13101302 1. 2
13101303 0. 4
13101400 -1
13101401 313. 313. 313. 313. 313.
13101402 330. 330. 330. 330. 330.
13101403 441. 441. 441. 441. 441.
13101404 445. 445. 445. 445. 445.
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13101406 454. 454. 454. 454. 454.
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13101410 468. 468. 468. 468. 468.
13101411 473. 473. 473. 473. 473.
13101412 473. 473. 473. 473. 473.
13101413 464. 464. 464. 464. 464.
13101414 449. 449. 449. 449. 449.
13101415 433. 433. 433. 433. 433.
13101501 0 0 0 1 4.0 3
13101502 0 0 0 1 8.0 14
13101503 0 0 0 1 4.0 15
13101601 310010000 10000 1 1 4.0 3
13101602 310040000 10000 1 1 8.0 14
13101603 310150000 0 1 1 4.0 15
13101701 777 .0 .0 .0 2
13101702 777 .0416666 .0 .0 3
13101703 777 .0833333 .0 .0 14
13101704 777 .0416666 .0 .0 15
13101901 0 .0118 .0 .0 15
*

```

```
* ***** * * ***** ***          ***   ***
*   *   * * *   * *   * *   * *   * *   * *
*   *   ***** ***** *****          ***** *****
*   *   * ' * *   * *   ** *   * *   * *   **
*   *   * *   ***** * *   ** *   * *   * *   **
```

*
*

```
20100100 TBL/FCTN 1 1          *BORONNITR.
20100101 20.0
20100151 3.22E+6
```

*

```
20100200 TBL/FCTN 1 1          *HEATER
20100201 16.7
20100251 3.266E+6
```

*

```
20100300 TBL/FCTN 1 1          *CLAD
20100301 273.15 12.9805 1199.82 25.1060 2000.0 25.1060
```

*

```
20100351 255.37 3561611. 422.04 3964814. 477.59 4099214.
20100352 533.15 4233615. 588.71 4334415. 644.26 4435081.
20100353 699.82 4502416. 810.93 4636816. 1366.48 5376019.
20100354 2000.00 5376019.
```

*

* TABLES

*

```
20277700 POWER 510 1. 1.
20277701 0.0 426. 14.5 426. 17.5 114805.3 587.5 115736.9
```

*

*CONTROL VARIABLES

*

20500100	COLLVL	SUM	1.0	0.0	1
20500101	0.0	0.125	VOIDF	310030000	
20500102		0.250	VOIDF	310040000	
20500103		0.250	VOIDF	310050000	
20500104		0.250	VOIDF	310060000	
20500105		0.250	VOIDF	310070000	
20500106		0.250	VOIDF	310080000	
20500107		0.250	VOIDF	310090000	
20500108		0.250	VOIDF	310100000	
20500109		0.250	VOIDF	310110000	
20500110		0.250	VOIDF	310120000	
20500111		0.250	VOIDF	310130000	
20500112		0.250	VOIDF	310140000	
20500113		0.125	VOIDF	310150000	
20500200	STEAM-OUT	MULT	.004785	0.0	1
20500201	VELGJ	410030000			
20500202	RHOGJ	410030000			
20500203	VOIDGJ	410030000			
20500300	WATER-OUT	MULT	.004785	0.0	1
20500301	VELFJ	410030000			
20500302	RHOFJ	410030000			
20500303	VOIDFJ	410030000			
20500400	WATER-IN	MULT	.004785	0.0	1
20500401	VELFJ	115000000			
20500402	RHOFJ	115000000			
20500403	VOIDFJ	115000000			
20500500	INJECTED	INTEGRAL	1.0	0.0	1
20500501	CNTRLVAR	4			
20500600	STEAM-OUT	INTEGRAL	1.0	0.0	1
20500601	CNTRLVAR	2			
20500700	WATER-OUT	INTEGRAL	1.0	0.0	1
20500701	CNTRLVAR	3			
20500800	MASS	SUM	1.0	0.0	1
20500801	0.0	1.0	CNTRLVAR		5
20500802		-1.0	CNTRLVAR		6
20500803		-1.0	CNTRLVAR		7

*

= REFLOOD EXP 3216

*

100 RESTART TRANSNT
101 RUN
103 54

*

*TIME STEPS

*

*	END	MIN	MAX	CTRL	MINED	MAJED	REST
201	550.0	.5E-4	.01	202	25	1000	1250

*

20800001 TREWET 3101
20800002 ZTRWT 3101

*

*MINOR EDITS

*

301 P 310010000
302 ZTRWT 3101
303 HTTEMP 310100505
304 HTTEMP 310100705
305 HTTEMP 310100905
306 HTTEMP 310101105
307 HTTEMP 310101305
308 HTTEMP 310101405

*

*TRIPS

*

501	TIME	0	GT	NULL	0	1000. N	*END
510	TIME	0	GT	NULL	0	0.0 L	*POWER
520	TIME	0	GT	NULL	0	0.0 L	*FILL FLOW
530	TIME	0	GT	NULL	0	.0 L	*REFLOOD
600	501						

*

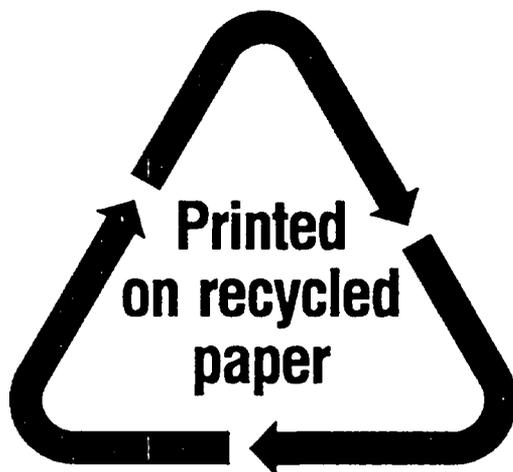
20501000 Q-FRONT SUM 1.0 0.0 1
20501001 -0.250 1.0 ZTRWT 3101

*

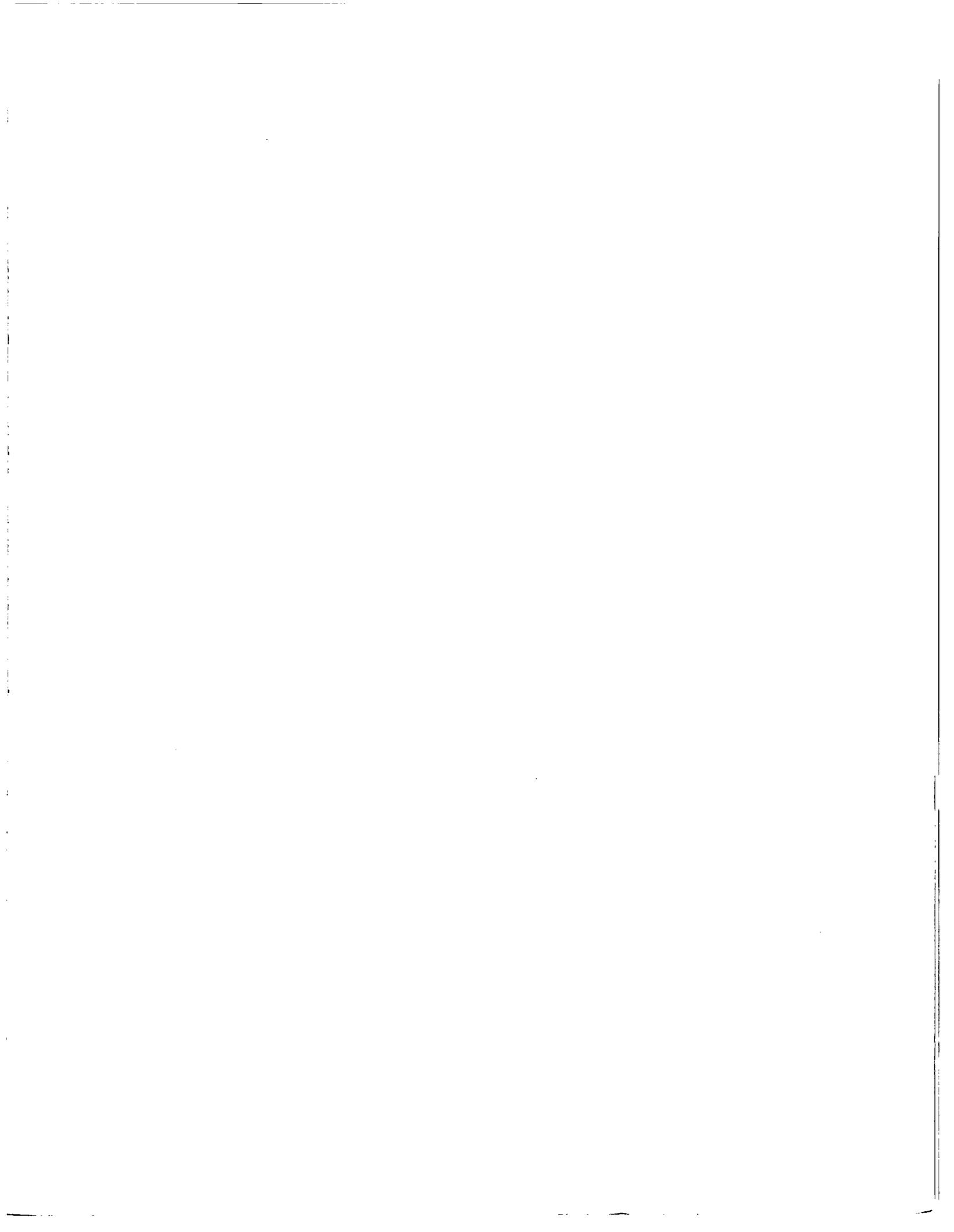
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	8. PERFORMING ORGANIZATION - NAME AND ADDRESS (If NRC, provide Division, Office or Region, U.S. Nuclear Regulatory Commission, and mailing address; if contractor, provide name and mailing address.) Netherlands Energy Research Foundation ECN Service Unit General Services P. O. Box 1, NL-1755 ZG Petten The Netherlands	
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11. ABSTRACT (200 words or less) As part of the ICAP (International Code Assessment and Applications Program) agreement between ECN (Netherlands Energy Research Foundation) and USNRC, ECN has performed a number of assessment calculations with the computer program RELAP5. This report describes the results as obtained by ECN from the assessment of the thermohydraulic computer program RELAP5/MOD2/CY 36.05 versus a series of reflood experiments in a bundle geometry. A total number of seven selected experiments have been analyzed, from the reflood experimental program as previously conducted by ECN under contract of the Commission of the European Communities (CEC). In this document, the results of the analyses are presented and a comparison with the experimental data is provided.		
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	14. SECURITY CLASSIFICATION <i>(This Page)</i> Unclassified <i>(This Report)</i> Unclassified	
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