

**SCCEX:**  
**A Computer Code for Substantially  
Complete Containment Example  
Analysis of a Reference Container**

**SCCEX: A COMPUTER CODE FOR SUBSTANTIALLY  
COMPLETE CONTAINMENT EXAMPLE ANALYSIS  
OF A REFERENCE CONTAINER**

*Prepared for*

**Nuclear Regulatory Commission  
Contract NRC-02-93-005**

*Prepared by*

**Center for Nuclear Waste Regulatory Analyses  
San Antonio, Texas**

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**Tony Y. Torng  
Peter C. Lichtner  
John C. Walton**

**Center for Nuclear Waste Regulatory Analyses  
San Antonio, Texas**

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## ABSTRACT

The Substantially Complete Containment EXample (SCCEX) computer code is designed to demonstrate an approach for evaluating containment by a waste package and to identify those areas that require more detailed analysis. Several models were coupled in the SCCEX code to calculate the time-to-wetting and the time-to-failure of waste packages for an unsaturated repository site. These models represent the repository thermal field, near-field environment, corrosion of container materials, including localized corrosion and stress corrosion cracking, and mechanical failures. This user manual discusses the models used in the SCCEX code, SCCEX code structure and capabilities, SCCEX code input and output files, SCCEX code baseline case, and configuration control requirements. This code is used in support of evaluating the "substantially complete containment" rule for waste packages in 10 CFR Part 60.

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## 1 INTRODUCTION

The objective of the Substantially Complete Containment EXample (SCCEX) code is primarily to demonstrate an approach for evaluating containment by a waste package and to identify those areas requiring more detailed analysis. SCCEX is not intended to demonstrate the suitability of any given waste package material or design in terms of performance requirements. For simplicity, the failure of a waste package in this analysis is defined as the condition of a waste package in which localized corrosion has penetrated the container walls, either by stress corrosion cracking or by mechanically dominated processes. The results obtained by this computer code will be used in evaluating the "substantially complete containment" rule for waste packages in the Code of Federal Regulations, Title 10, Part 60 (10 CFR Part 60).

The code is based on the reference waste package design presented in the Site Characterization Plan (SCP) (U.S. Department of Energy, 1988). The waste package consists of a relatively thin-walled, corrosion-resistant metal container placed in an oversized vertical borehole in the repository. The geometry has been simplified to permit the use of simple analytical expressions for the application of the various mechanical models used in the code. The container materials conform generally to the austenitic alloys described in the SCP. However, the code has significant departures in the assumptions on the chemical and loading environments from those described in the SCP.

The modeling of the near-field environment used in the code is focused on the time-dependent evolution of the chemical environment on the waste package surface. This focus is particularly important in the case of an unsaturated site, where the potential exists for groundwater to drip on a thermally hot waste package and subsequently, on evaporation, to deposit salts on the waste package surface. This concentration of salts in the presence of future groundwater intrusion can promote and accelerate the corrosion of certain waste package materials. Due to the simplified nature of the models on which the code is based and the assumptions and approximations made, the code does not necessarily provide a quantitative representation of the actual conditions that may be presented in an unsaturated repository site.

Brief overviews of the repository thermal field, near-field environment, corrosion mechanisms of container materials, including localized corrosion and stress corrosion cracking, as well as mechanical failures models embodied in the SCCEX Version 1.0 software are provided in Section 2. Section 3 contains a general description of the SCCEX software. The required input parameters for the SCCEX code are discussed in Section 4, and the corresponding output files are discussed in Section 5.

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## 2 BRIEF DESCRIPTION OF MODELS

### 2.1 OVERVIEW

The SCCEX code, developed to assess the containment of high-level waste (HLW) in a waste package, involves the use of several computation models that are interconnected both spatially and temporally in a geologic repository. In the following subsections, a brief description of these models, which include the repository thermal field, near-field environment, corrosion of container materials, including localized corrosion and stress corrosion cracking, as well as mechanical failures models is provided. More detailed rationale, descriptions, and limitations of the various models can be found in the Engineered Barrier System Performance Assessment Codes (EBSPAC) progress report (Sridhar et al., 1993) and the report entitled "Substantially Complete Containment" — Example Analysis of a Reference Container (Cragolino et al., 1994). This section is essentially a summary of the description presented in the latter report (Cragolino et al., 1994).

### 2.2 THERMAL MODEL

The thermal model is based on heat conduction as the only heat-transfer mechanism. The repository is considered to be a volumetric source with a square shape having a uniform and constant thermal conductivity and heat capacity. For a rectangular repository, the temperature field for a homogeneous, isotropic, and an infinite three-dimensional medium is given in terms of the Green's functions as shown below:

$$G = \frac{(G_x G_y G_z)}{8\rho C_p w^2 h} \quad (2-1)$$

$$G_x = \text{Erf} \left( \frac{\frac{w}{2} + x}{\sqrt{4\alpha t}} \right) + \text{Erf} \left( \frac{\frac{w}{2} - x}{\sqrt{4\alpha t}} \right)$$

$$G_y = \text{Erf} \left( \frac{\frac{w}{2} + y}{\sqrt{4\alpha t}} \right) + \text{Erf} \left( \frac{\frac{w}{2} - y}{\sqrt{4\alpha t}} \right) \quad (2-2)$$

$$G_z = \text{Erf} \left( \frac{\frac{h}{2} + z}{\sqrt{4\alpha t}} \right) + \text{Erf} \left( \frac{\frac{h}{2} - z}{\sqrt{4\alpha t}} \right)$$

where

- $\rho C_p$  = volumetric heat capacity
- $w$  = width of square repository

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- $h$  = height of repository
- $x, y, z$  = distance from center of repository (assumed zero)
- $\alpha$  =  $\kappa / \rho C_p$  = thermal diffusivity
- $\kappa$  = thermal conductivity

The time and spatially dependent temperature is obtained from a convolution integral with the heat generation rate

$$T(x, y, z, t) = \left[ \int_0^t Q(\tau) m G(t - \tau) d\tau \right] + T_{ref} \quad (2-3)$$

where

- $t$  = time
- $Q$  = heat generation rate per kg of initial heavy metal
- $m$  = amount of heavy metal
- $T_{ref}$  = initial temperature (23 °C)

The rate of heat generation ( $Q$ ) is based upon data reported by the U.S. Department of Energy (1993). In addition to the overall heating of the repository, the temperature difference between the surface of the waste package and the rock some distance away is modeled using a steady-state, heat-conduction model for a radial geometry. The quasi-steady-state assumption for variation of the temperature is used because the overall repository temperature decreases much more slowly as a result of the radioactive decay than local (waste package scale) temperature changes due to conduction over relatively short distances. The quasi-steady-state temperature difference between the surface of a container and the rock some distance away is given by

$$\Delta T = \frac{mQ}{2\pi l} \left[ \frac{\ln\left(\frac{r_2}{r_1}\right)}{\kappa_p} + \frac{\ln\left(\frac{r_3}{r_2}\right)}{\kappa_r} \right] \quad (2-4)$$

where

- $r_1, r_2, r_3$  = radial distance of container wall, packing/rock interface, and outer boundary respectively from container centerline
- $\kappa_p, \kappa_r$  = thermal conductivity of packing and rock, respectively
- $l$  = length of container

The output of this model is the temperature distribution in Cartesian coordinates from the centerline of the repository and the temperature drop between an individual container and the surrounding rock at an assumed distance for any given time period. A significant limitation of the expression for the temperature drop,  $\Delta T$ , is that it increases without bound as the radius parameter,  $r_3$ , of the outer boundary increases. Unrealistic results may be obtained if the value used for  $r_3$  becomes too large. There is no check of this in the code and the user must evaluate the results to make certain they are reasonable. Furthermore, the results are generally sensitive to the value of  $r_3$  chosen.

### 2.3 ENVIRONMENTAL MODEL

In the environmental model, the evolution of the environment on the waste container surface is computed. The environment around the container is dictated by the evaporation rate of water contacting the container, the influx rate of water, the types of salts precipitated, and their effects in reducing the vapor pressure of water on the container surface, which promotes movement of water vapor to or away from the container surface. The results of this model are the time at which a water film is stabilized on the container (time-to-wetting or wetting time), the thickness of the scale layer precipitated on the container surface, the area covered by a water film on the surface of the container, and the concentration of ionic species in the water film. It is assumed that the water film has a limited thickness. The wetted area is calculated from the volume of water available at the container surface using an arbitrary value for the thickness of the water film.

Several factors are calculated by solving a set of ordinary differential equations representing conservation of mass. These factors include the amount of water on the container surface, the amount of scale deposited, the amount of effluent generated, the amount of soluble salts on the container surface, and the depth of penetration by corrosion. The material balance equations are given by

$$\frac{dV}{dt} = Q_{in} - Q_{out} - \frac{EM_{H_2O}}{\rho_{H_2O}} \quad (2-5)$$

$$\frac{ds}{dt} = C_{in}^s Q_{in} - C_{out}^s Q_{out} \quad (2-6)$$

$$\frac{dS}{dt} = C_{in}^S Q_{in} - C_{out}^S Q_{out} \quad (2-7)$$

$$\frac{d\Gamma}{dt} = Q_{out} \quad (2-8)$$

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$$\frac{dL}{dt} = r \quad (2-9)$$

where

- $V$  = volume of water on waste container surface
- $Q_{in}, Q_{out}$  = volumetric flow rate of water onto and exiting the waste container surface
- $E$  = molar evaporation rate from the entire container surface without end effects
- $M_{H_2O}$  = molecular weight of water
- $\rho_{H_2O}$  = density of water
- $S$  = mass of soluble salts on container surface
- $s$  = mass of scale-forming compounds on container surface
- $C_{in}, C_{out}$  = input and output aqueous concentration of soluble salts or scale-forming compounds
- $\Gamma$  = cumulative amount of effluent water
- $L$  = depth of penetration by corrosion
- $r$  = corrosion rate, either passive or active

When the container is completely covered with water, the steady-state conditions correspond to  $dV/dt=0$ , and  $Q_{out}$  is given by the difference between  $Q_{in}$  and the evaporation rate.

Liquid water can reach the container surface by several mechanisms including matrix flow, fracture flow, or condensate dripping. Water flow on the container is not calculated in the SCCEX code, but it can be specified by two different options. The first option is to directly input the Darcy velocity near the container as a function of time in tabular format. The flow onto the container surface is then the input flow rate multiplied by the representative area of the individual waste package multiplied by an input factor specifying the proportion of water passing a waste package that actually drips onto the container surface and the evaporation rate.

The second option is more complex and assumes a larger scenario. The imagined scenario is the drying of the repository by the thermal loading. The concept has been assumed to be a hydrothermal umbrella protecting the repository. The hydrothermal umbrella tends to protect the portions of the repository heated above the boiling point of water from water dripping onto the containers. As a result of the umbrella, the flux of water onto the repository is diverted around the center of the repository to the outer edges, which have temperatures below the boiling point of water. Further from the edge of the umbrella, the downward flux of water reverts to the input (background) flow rate. This scenario is implemented in the code relative to an input temperature specified at the edge of the umbrella, along with

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a positive or negative variation within a specified range. The physical thickness of the umbrella edge (where enhanced flow occurs) and the surface area of impingement are also inputs to the code.

Below the boiling point of the solution, the rate of evaporation is a function of overall temperature and temperature drop between the container and surrounding rock. The flux equation for binary diffusion of water vapor through air, assuming infinite permeability of the medium (i.e., constant pressure), is given by Bird et al. (1960).

$$N_{H_2O} = x_{H_2O}(N_{H_2O} + N_{air}) - cD\tau\phi\nabla x_{H_2O} \quad (2-10)$$

where

- $N_{H_2O}$  = molar flux of water vapor
- $N_{air}$  = molar flux of air
- $x_{H_2O}$  = mole fraction of water vapor
- $c$  = total molar concentration of gas
- $D$  = binary diffusion coefficient
- $\tau$  = tortuosity factor
- $\phi$  = rock porosity

Steady-state evaporation in a radial geometry gives

$$E = 2\pi lcD\tau\phi \frac{\ln\left(\frac{1-x_1}{1-x_3}\right)}{\ln\left(\frac{r_1}{r_3}\right)} \quad (2-11)$$

where

- $E$  = molar evaporation rate from the entire container surface without end effects
- $x_1, x_3$  = mole fraction of water vapor at container surface and at distance, respectively

The tortuosity and porosity factors are treated as independent parameters. The diffusion coefficient in the air/water vapor system in  $m^2/s$  is assumed to be given by Treybal (1980).

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$$D = 3.05 \times 10^{-5} \left( \frac{760}{680} \right) \left( \frac{T}{T_{ref}} \right)^{1.5} \quad (2-12)$$

where the pressure at the repository horizon is taken as 680 mm Hg, and the reference temperature  $T_{ref} = 232 \text{ }^\circ\text{K}$  ( $59 \text{ }^\circ\text{C}$ ). The vapor pressure of water as a function of temperature is taken from Perry's Handbook (Perry and Chilton, 1973). Conversions between vapor pressure, concentration, and mole fraction are performed with the ideal gas law.

Heat loading, combined with limited water supply, leads to creation of a desiccated zone around the waste package in which the relative humidity is decreased well below one. Three conditions can cause water to be present within this zone: (i) adsorbed or capillary water, (ii) solute-caused lowering in vapor pressure, and (iii) transient water related to fracture drainage. Vapor pressure lowering in capillaries,  $b_{capillary}$ , is described with Kelvin's equation.

$$b_{capillary} = \frac{P_{capillary}}{p^0} = \exp \left[ \frac{\psi M_{H_2O} g}{RT} \right] \quad (2-13)$$

where

- $P_{capillary}$  = vapor pressure of capillary
- $p^0$  = vapor pressure at temperature for pure water.
- $\psi$  = matrix potential
- $g$  = acceleration of gravity
- $R$  = gas constant
- $T$  = temperature

Vapor pressure lowering from solutes,  $b_{solute}$ , is a function of concentration and solute composition according to

$$b_{solute} = \left( \frac{p_{solute}}{p^0} \right) = f(C_1, C_2, \dots, C_i) \quad (2-14)$$

where  $f$  represents an arbitrary function of the solution composition specified by concentration  $C_i$  of the  $i$ th species. Total vapor pressure lowering is a combination of solute and capillary effects given by the equation

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$$\frac{P_{total}}{p^0} = b_{capillary} \cdot b_{solute} \quad (2-15)$$

In the code, the salt that is precipitated is assumed to be sodium chloride. Based on this assumption, the time-to-wetting is calculated by assuming that wetting occurs when the temperature of the container is such that a saturated solution of NaCl can become thermodynamically stable as a liquid film on the container surface at a temperature higher than the boiling temperature of pure water. The vapor pressure of water in the saturated solution on the container surface is then lower than the vapor pressure of pure water at the outer boundary temperature. The assumed chemical composition (i.e., saturated chloride solution) is then used as input to the corrosion model.

## 2.4 RELEASE RATE

Release rate is simulated for a single, highly soluble, radionuclide such as iodine or technetium. Integration of the release equations is dependent upon location in time. Three time periods are identified. Prior to container failure, the spent fuel remains intact, and the radioactive decay is the only active process. Container failure cannot occur until the surface of the container is wetted. In the simulations presented in this paper, the container is assumed to fail immediately upon wetting. The rate of change for each variable during this period is:

$$\begin{aligned} \frac{d\gamma_1}{dt} &= -\lambda\gamma_1 \\ \frac{d\gamma_2}{dt} &= 0 \\ \frac{d\gamma_3}{dt} &= 0 \end{aligned} \quad (2-16)$$

After the waste container fails, spent fuel alteration begins. The governing equations during this alteration period are

$$\begin{aligned} \frac{d\gamma_1}{dt} &= -\lambda\gamma_1 - (\text{alt}) \exp[-\lambda t] \\ \frac{d\gamma_2}{dt} &= (\text{alt}) \exp[-\lambda t] - Q_{out} \frac{\gamma_2}{V} - \lambda\gamma_2 \\ \frac{d\gamma_3}{dt} &= Q_{out} \frac{\gamma_2}{V} \end{aligned} \quad (2-17)$$

Beyond the alteration period, the governing equations are

$$\frac{d\gamma_1}{dt} = 0$$

$$\frac{d\gamma_2}{dt} = -Q_{out} \frac{\gamma_2}{V} - \lambda \gamma_2 \tag{2-18}$$

$$\frac{d\gamma_3}{dt} = Q_{out} \frac{\gamma_2}{V}$$

where

- $\gamma_1$  = proportion of initial radionuclide inventory remaining in the unaltered spent fuel
- $\gamma_2$  = proportion of initial radionuclide inventory dissolved in the water inside the failed waste package
- $\gamma_3$  = proportion of initial radionuclide inventory released from waste package
- $\lambda$  = radionuclide decay rate ( $yr^{-1}$ )
- $alt$  = alteration rate of spent fuel into secondary minerals ( $yr^{-1}$ )

The period of alteration extends from the failure time (*tfail*) to *tfail*+1/*alt*. The assumption is made that, prior to the time of leachate generation from the waste package, liquid water flow is always towards the waste package, effectively preventing diffusional and advective releases in the liquid phase (Pruess and Tsang, 1993). Final release from the waste package is assumed to be advectively controlled.

## 2.5 CORROSION MODEL

The corrosion model in the SCCEX code calculates the rates of uniform corrosion, localized corrosion, and stress corrosion cracking. The corrosion process at any given time period is dictated by the corrosion potential and the appropriate critical potential for a given corrosion process.

### 2.5.1 Corrosion Potential

Two cathodic reactions are modeled in the code: oxygen reduction and hydrogen evolution reactions. The oxygen reduction reaction is assumed to be a mixture of activation-controlled charge transfer process and molecular diffusion-controlled transport process. The resulting current density can be written as

$$i_{O_2} = -k_{O_2} C_{O_2}^{bulk} \frac{\exp\left(-\frac{z_{O_2} \beta FE_{corr}}{RT}\right)}{\left[1 + \frac{k_{O_2} \delta \exp\left(-\frac{z_{O_2} \beta FE_{corr}}{RT}\right)}{4FD_{O_2} \tau \phi}\right]} \tag{2-19}$$

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where

$k_{O_2}$  = reaction rate constant for the oxygen reduction reaction

$E_{corr}$  = corrosion potential

$F$  = Faraday constant

$\alpha$  = charge transfer coefficient

$\beta$  =  $1 - \alpha$

$R$  = gas constant

$T$  = temperature in °K

$z_{O_2}$  = number of electrons involved in the process per mole

$D_{O_2}$  = diffusivity of oxygen in aqueous solution

$\tau$  = tortuosity

$\phi$  = porosity

$\delta$  = thickness of the diffusion layer (e.g., scale or water film)

$C_{O_2}^{bulk}$  = bulk concentration of oxygen in solution.

For the oxygen reduction reaction, the bulk concentration is related to the partial pressure through Henry's law

$$C_{O_2}^{bulk} = K_H \cdot p_{O_2} \quad (2-20)$$

where  $p_{O_2}$  is the partial pressure of oxygen over the solution and  $K_H$  is the Henry's law constant for oxygen solubility. The corrosion potential,  $E_{corr}$ , is defined as the potential at which the current due to all the cathodic processes is equal to the current due to all the anodic processes including the electrochemical dissolution of the metal.

The reaction rate constant is calculated from the exchange current density using the following equation

$$i_{O_2}^0 = k_{O_2} C_{O_2}^{bulk} \exp \left( - \frac{z_{O_2} (1 - \alpha) F}{RT} E_{eq}^{O_2} \right) \quad (2-21)$$

where

$i_{O_2}^0$  = exchange current density

$E_{eq}^{O_2}$  = equilibrium potential for the oxygen evolution reaction

For the hydrogen evolution reaction or the water reduction reaction, the cathodic current is assumed to be dictated only by the charge transfer process. The cathodic current density is given by

$$i_{H_2O} = -k_{H_2O} \left[ \exp \left( - \frac{\beta_{H_2O} z_{H_2O} F}{RT} E_{corr} \right) \right] \quad (2-22)$$

where

- $k_{H_2O}$  = reaction rate constant for the water reduction reaction
- $E_{corr}$  = corrosion potential

The reaction rate constant can be calculated from the appropriate exchange current density for the hydrogen evolution reaction similar to that shown in Eq. (2-21). The equilibrium potential for water reduction/hydrogen evolution will depend on the bulk concentration of the  $H^+$  ion, which is related to the pH. The temperature dependence of the reaction rate constants for the oxygen evolution and the water reduction reactions are assumed to be given by an Arrhenius-type relationship as shown in Eq. (2-23).

$$k = k_{298 \text{ } ^\circ K} \exp \left[ \frac{E_a}{R} \left( \frac{1}{298} - \frac{1}{T} \right) \right] \quad (2-23)$$

where  $E_a$  is the activation energy for the particular cathodic reaction and  $k_{298 \text{ } ^\circ K}$  is the reaction rate constant at 298 °K. The anodic current is assumed to be equal to the passive current density of the alloy and to be independent of the potential. The corrosion potential is then calculated by solving simultaneously for  $E_{corr}$  using Eqs. (2-19), (2-22), and the equality of anodic and cathodic current.

### 2.5.2 Critical Potentials for Pitting, Crevice Corrosion, and Stress Corrosion Cracking

Empirically derived equations are used in the SCCEX code for the dependence of critical potentials on environmental parameters. The pit initiation and repassivation potentials are assumed to depend only on the chloride concentration and temperature. However, in the current calculations, the effects of these anionic species are not considered. The dependence of the critical potentials on chloride concentration and temperature is given by

$$E_{crit} = A(T) + B(T) \log [Cl^-] \quad (2-24)$$

where the constants  $A(T)$  and  $B(T)$  were considered as linear functions of temperature. The constants were evaluated from literature and the CNWRA data for initiation and repassivation potentials for both pitting and crevice corrosion (Sridhar et al., 1993).

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The existence of a critical potential for stress corrosion cracking is less certain; however, it was assumed to be equal to the repassivation potential for localized corrosion. Justification for this assumption can be found in recent investigations (Tamaki et al., 1990; Tsujikawa et al., 1994) as discussed previously by Sridhar et al. (1993).

## 2.6 MECHANICAL MODEL

The SCCEX code includes three mechanical failure models: buckling, yielding, and fracture. Simplified analytical models were developed to convert a seismic-type load to a pseudostatic pressure acting on the curved shell surface of a container emplaced in an oversized vertical borehole. To generate the seismic load, it was assumed that the peak seismic acceleration would cause the container mass to impact the top part of the wall of the borehole. Further, it was assumed that there were no momentum losses in the impact and the bottom of the container moved on a frictionless surface. In the calculations involving seismic load, the region of contact with the borehole is assumed to be 10 percent of the circumference of the container. This assumption is conservative, considering that the entire impact load of the container is applied to a limited part of the container surface. Based on the peak acceleration, a uniform pressure,  $q$ , was calculated and used in the different mechanical models. In the current SCCEX code, an acceleration of 0.4 g seismic load was used.

### 2.6.1 Buckling Failure Model

The model used in the analysis for buckling is described in Sridhar et al. (1993). In this model, a shell buckling case is considered. The analytical equation used for this buckling failure model is expressed as

$$R_B = \frac{99Et_R^3\pi}{60r^2(1 - \nu^2)} \quad (2-25)$$

where

- $R_B$  = residual buckling load capacity for the container
- $E$  = Young's Modulus
- $\nu$  = Poisson's ratio
- $r$  = inner radius of the container
- $t_R$  = remaining thickness at any given time after accounting for corrosion of the container

It should be noted that the constants in the expression are based on the initial thickness-to-radius ratio of the container being 1:10. A safety factor equal to two was used for this failure model to add conservatism.

### 2.6.2 Yield Failure Model

The residual yield capacity,  $R_Y$ , was determined (Sridhar et al., 1993) from the following equation

$$R_Y = R_{YO} \frac{A_R}{A} = R_{YO} \frac{t_R}{t} \quad (2-26)$$

where

- $R_{YO}$  = yield strength of the material
- $A$  = initial cross section area of the solid part of the cylinder
- $A_R$  = remaining cross section area of the solid part of the cylinder
- $t$  = initial thickness of the cylinder
- $t_R$  = remaining thickness of the cylinder after corrosion

A safety factor of two was also incorporated into Eq. (2-26) to permit conservative calculations.

### 2.6.3 Fracture Failure Model

The conceptual model for developing the stresses for fracture is the same as that described in the previous subsection. The fracture model is expressed (Sridhar et al., 1993) as

$$R_F = \frac{K_{IC}}{Y(\pi a)^{0.5}} \quad (2-27)$$

where

- $R_F$  = permissible external stress
- $Y$  = geometry factor
- $a$  = crack depth or the depth of a corroded pit
- $K_{IC}$  = fracture toughness

A safety factor of two was used for this failure model to account for added conservatism.

### 2.6.4 Time-Dependent Thickness Models

An important parameter used in the buckling failure model and the stress computations is the time-dependent thickness of the container wall (Cragolino et al., 1994). It should be noted that the wall thickness is reduced as a result of general or local corrosion. In the case of general corrosion, the thickness is assumed to decrease uniformly with time. However, for localized corrosion effects, the reduction of thickness is not uniform.

### 3 SOFTWARE DESCRIPTION

#### 3.1 SCCEX CODE CAPABILITIES

In general, the SCCEX code involves the following calculations:

- (i) Calculate the average repository temperature as a function of time using a convolution integral with a Green's function solution to the conduction equation.
- (ii) Calculate the difference in temperature between the container and the rock at a distance specified as an input parameter. In addition, the evaporation rate of pure water from the container surface (i.e., evaporation assuming the container is always covered with pure water) is calculated for placing predicted evaporation rates in perspective.
- (iii) Solve a system of ordinary differential equations for
  - Volume of water on container surface (m<sup>3</sup>)
  - Mass of salts on container surface (kg)
  - Depth of corrosion (m)
  - Volume of effluent water leaving container (m<sup>3</sup>)
  - Mass of scale on container (kg)

This step is the most computationally intensive portion of the code.

- (iv) Estimate the release for a single radionuclide. The radionuclide is assumed to be highly soluble. Three differential equations are solved: (a) proportion of the initial inventory of the radionuclide remaining in the waste, (b) proportion of the initial inventory in the waste package water, and (c) proportion of the initial inventory released from the waste package.
- (v) Estimate the salinity inside a failed waste container assuming vapor/liquid equilibrium.

#### 3.2 SCCEX CODE STRUCTURE

The SCCEX code flow diagram is presented in Figure 3-1. The input data required to execute the SCCEX code include the following: (i) total simulation time, (ii) geometry of container, (iii) temperature parameters, (iv) evaporation parameters, (v) solver selection and related parameter, and (vi) corrosion parameters. The input and output structure for the SCCEX code will be discussed in detail in the following subsections. The idealized repository is assumed to be a square area with an assumed one-eighth symmetry for the temperature field containing equally spaced waste packages. Based on the symmetry, the SCCEX code divides the repository into calculation cells. A typical cell structure for the repository is shown in Figure 3-2. In the SCCEX code, the calculation cells on the diagonal occur four times in the repository, whereas off-diagonal cells occur eight times. The number of times each cell occurs in the repository is called the weighing factor, which is used to calculate the total number of failures in the repository.

For each cell, the calculations begin with an estimate of thermal loading and resulting temperature effects. The average repository temperature, the container surface temperature, and the container internal temperature are calculated as a function of time and stored in arrays. In a later section of the code, the thermal calculations are combined with water drip rates to estimate the amount of water on the container surface and its composition.

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**Figure 3-1. Flow diagram of the SCCEX code**

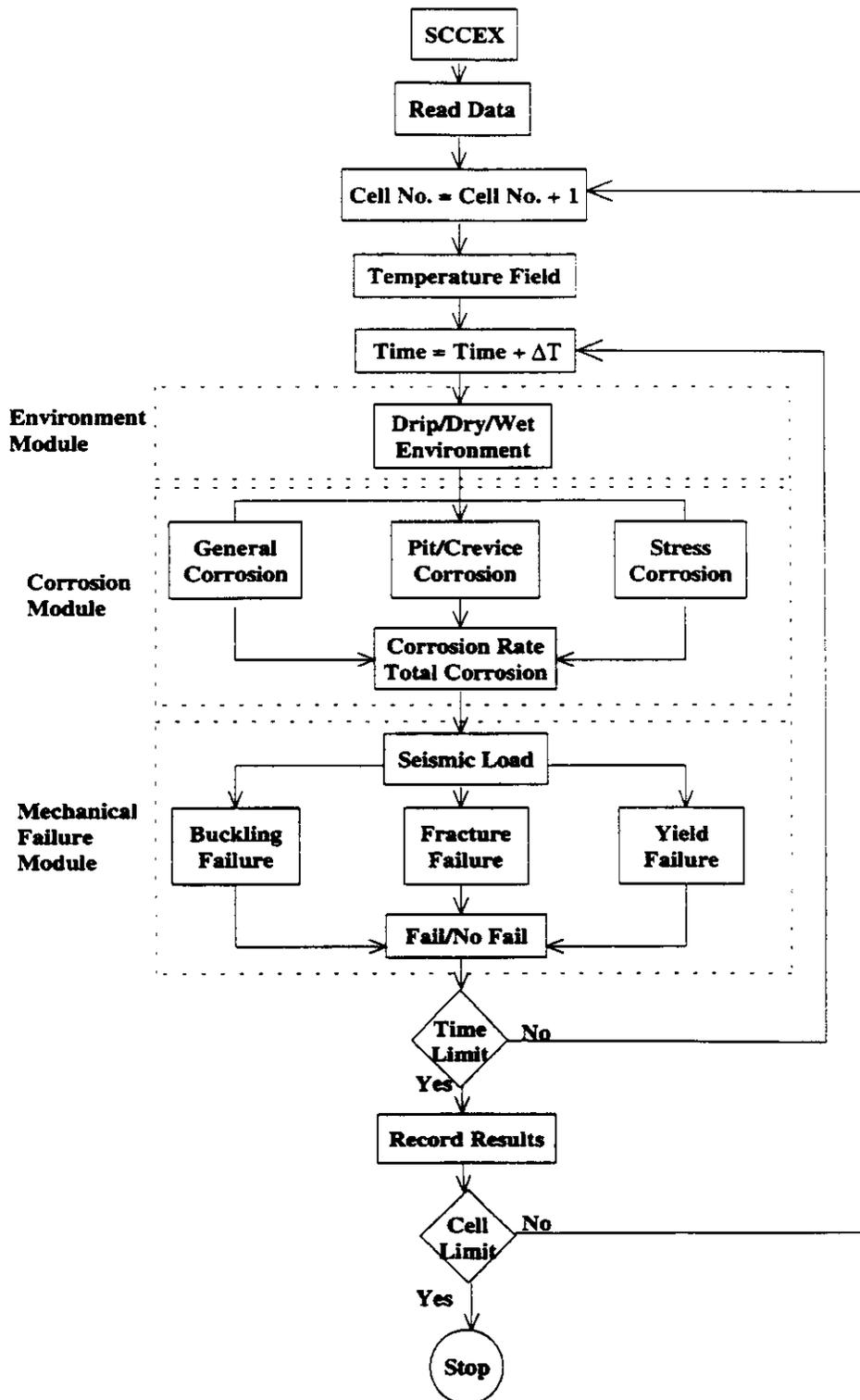


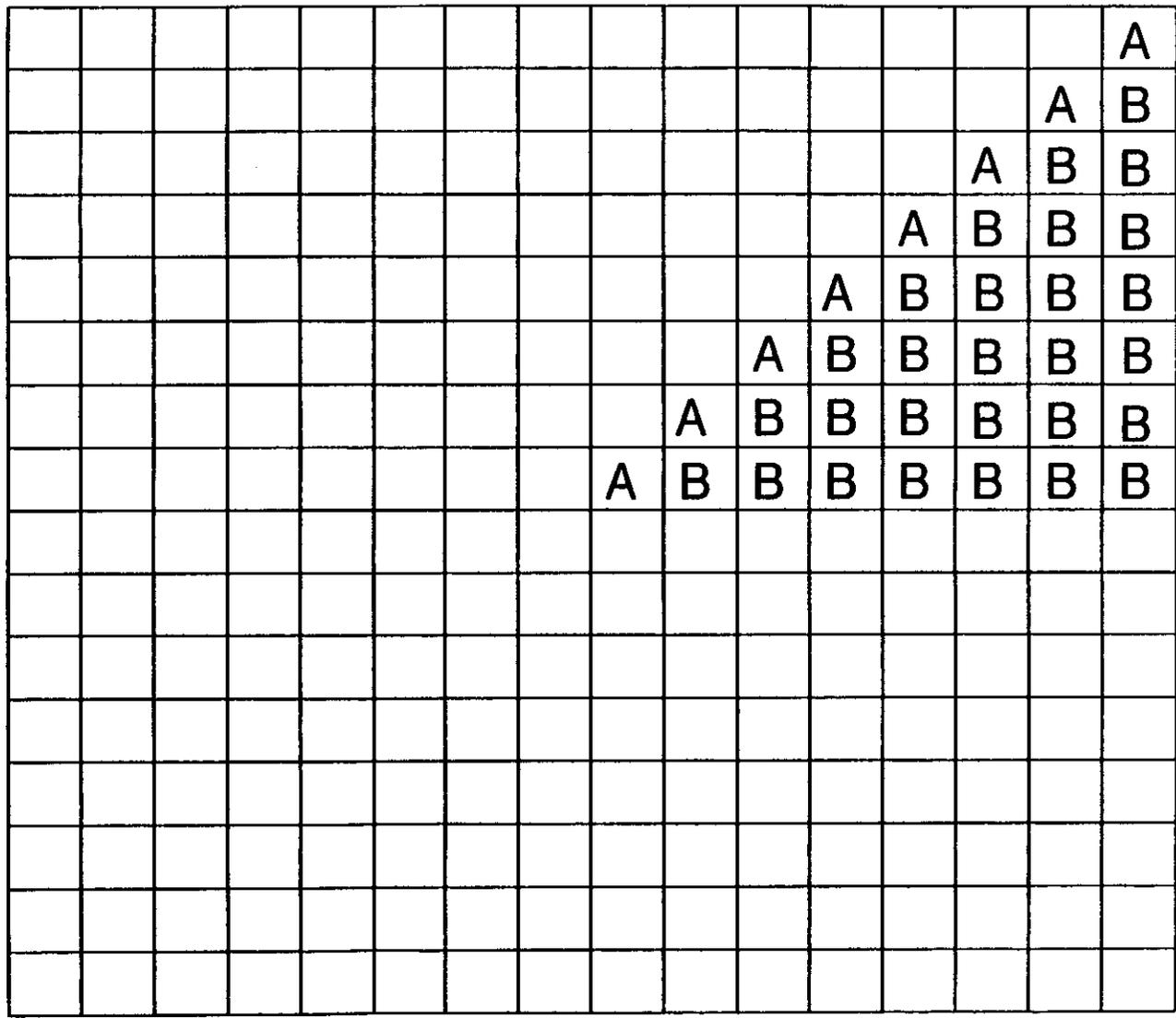
Figure 2-1. Flow diagram of the SCCEX code

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**Figure 3-2. Definition of repository cells and groups**

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16 x 16



Note: A = 4 cells, B = 8 cells, modeled as 1/8 symmetry

Figure 2-2. Definition of repository cells and groups

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Based on the calculated water composition and temperature, either general corrosion, pit/crevice corrosion, or stress corrosion cracking may take place, and the corresponding corrosion rates are estimated. The container temperature, corrosion penetration depth, and area penetrated by corrosion are then used to assess the structural integrity of the container. The residual strengths of buckling, fracture, and yield are then compared with a deterministic seismic-induced stress to determine if a mechanical failure occurs. The above process is repeated incrementally until the end simulation time has been reached. Selected calculational results such as the time-to-wetting and time-to-failure are stored in output files.

Data are read in from an input deck and written to several output files (simple, main, summary, and mechanical). Brine.f is the main program that controls the flow of all calculations. Subroutines are in files: input.f, lsodes.f, ode.f, and subroutines.f. In addition, some common blocks are stored in files: bulk.f, ecorr.f, hist.f, solve.f, vapor.f, and watt.f. These common blocks are used to store data that do not generally change. This storage reduces the potential for errors in the input deck. The functions of these files are summarized in Table 3-1.

**Table 3-1. Function of SCCEX Files**

Name	Function
brine.f	controls the flow of all calculations
input.f	read in data from UNIX standard input format
lsodes.f	package for solving ordinary differential equations
ode.f	routines for solving ordinary differential equations from numerical recipes
subroutines.f	this file contains several important subroutines: <ol style="list-style-type: none"> <li>1. rate: calculate derivatives for the main calculations.</li> <li>2. derivs: calculate derivatives for the repository source.</li> <li>3. green: calculate Green's function for parallel piped heat source.</li> <li>4. power: calculate the power in J/yr per metric ton of initial metal.</li> <li>5. corrode: calculate the corrosion rate and corrosion potential.</li> <li>6. lint: perform linear interpolation</li> <li>7. block data a: initialize vapor pressure arrays</li> <li>8. block data b: data for power generation</li> <li>9. function erf: calculate error function</li> <li>10. ratint: interpolate rate data</li> <li>11. drip: calculate flow rate of water on the container as a function of time.</li> <li>12. release: calculate derivative for radionuclide release.</li> </ol>
ecorr.f	corrosion potential variables (common block)
hist.f	time history variables and number of print time steps (parameter statement)
solve.f	variables pertinent to numerical solvers (common block)
vapor.f	vapor pressure information (parameter statement)
watt.f	thermal loading data (parameter statement)
bulk.f	common block and parameter statement

### 3.3 SCCEX CODE COMPILATION AND LINKING

SCCEX code is written in standard FORTRAN 77 with real\*8 (double precision) variables. On the Sun workstation platform or any UNIX operating system, to compile and link the SCCEX code, the easiest way is to create a makefile. The current makefile used on the Sun workstation shown in Table 3-2.

Table 3-2. Makefile for SCCEX Code

```

brine.e :    brine.o ode.o input.o subroutines.o lsodes.o mech.o
           f77 -w -O4 -o brine.e brine.o ode.o input.o subroutines.o mech.o lsodes.o
brine.o :    brine.f bulk.f hist.f ecorr.f solve.f
           f77 -w -O4 -c  brine.f
ode.o :      ode.f
           f77 -w -O4 -c  ode.f
input.o :    input.f bulk.f hist.f ecorr.f solve.f
           f77 -w -O4 -c  input.f
subroutines.o :    subroutines.f bulk.f hist.f ecorr.f solve.f
           f77 -w -O4 -c  subroutines.f
lsodes.o :   lsodes.f
           f77 -w -O4 -c  lsodes.f
mech.o :     mech.f bulk.f
           f77 -w -O4 -c  mech.f

```

where -w is used to suppress warning message, -O4 is used to optimize the code using the optimization level 4, -o is used to name the executable file, brine.e, and -c are used to compile without linking.

### 3.4 HARDWARE REQUIREMENTS AND INSTALLATION PROCEDURE

The SCCEX code was originally designed to run on any platform supporting standard FORTRAN 77. Total lines for the SCCEX code is around 8,186 lines. The largest five arrays used in the SCCEX code are 300x100 in size; the rest of the arrays are vectors that are less than 1000 in size. Therefore, total memory required for this SCCEX code should be less than 1.5 Mb.

Before running the SCCEX code, two steps must be taken. The first step consists of removal of any files that may conflict with the SCCEX system output file names. Secondly, the input file must be prepared for the run of interest.

To execute the SCCEX code on a UNIX system, the following command statement can be executed:

```
%brine.e < input filename > output filename
```

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### 3.5 USER SUPPORT

For technical assistance, contact:

Center for Nuclear Waste Regulatory Analyses  
Southwest Research Institute  
P. O. Drawer 28510  
San Antonio, TX 78228-0510

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## 4 INSTRUCTIONS FOR INPUT DATA

### 4.1 OVERVIEW

The parameters included in the SCCEX code input file for the different calculations and models were selected from applicable data available in the literature or estimated for particular processes (i.e., binary diffusion of water vapor through air, oxidation rate in air) on the basis of approximations to similar cases. Most of the parameters referring to the dimensions of the container and thermal properties for the near-field environment were obtained from the SCP for the proposed repository at Yucca Mountain (U.S. Department of Energy, 1988). Detailed discussion for the input data selected in this report have been summarized by Cragnolino et al. (1994).

In the following subsections, the required input data for simulation time and reference container geometry, thermal model, environmental model, release rate and solver parameters, corrosion model, and mechanical model will be briefly discussed. In addition, the baseline input data selected will also be illustrated.

### 4.2 SIMULATION TIME AND REFERENCE CONTAINER GEOMETRY INPUT

In the input file, the first block of data describes the simulation and reference container geometry information as follows:

Line

No.

- 1 Title line for this input file
- 2 Total simulation time (in yr)  
- Variable *tend*
- 3 Container x,y,z location (in m), number of cells (must be a power of 4)  
- Variables *x, y, z, ncell*
- 4 Container length (l), container radius (r1), borehole radius+gap (r2), outer boundary (r3) (all in meters)  
- Variables *rlen, r1, r2, r3*
- 5 Container thickness (in m)  
- Variable *cthick*

For the baseline case, this block of data are listed as follows:

Line

No.

- 1 This is the Brine or SCCEX code input file ! title line
- 2 1000. ! total simulation time
- 3 0., 0., 0., 4 ! container x,y,z location, number of cells
- 4 4.76, 0.33, 0.34, 5.0 !container length, container radius, borehole radius, outer boundary
- 5 0.01 ! container thickness in m

Note that this input file is read in a free-format fashion. Text following the exclamation point is treated as a comment. Comments must appear on the same line as the exclamation point. The same format is used for the other subsections.

### 4.3 THERMAL MODEL INPUT

The second block of data describes the thermal model as follows:

- Line No.
- 6 Title line for thermal input
- 7 Initial power density (in J/yr/m<sup>2</sup>)  
- Variable *powden*
- 8 Metric ton initial heavy metal (MTIHM) total (in tons), MTIHM per container or canister (in tons), age of fuel (in yr)  
- Variables *tons, canld, age*
- 9 Thermal conductivity of rock ( $\kappa_r$ ), packing ( $\kappa_p$ ), container or canister (in J/yr/m/K)  
- Variables *tkr, tkp, tk*
- 10 Volumetric heat capacity for rock ( $\rho C_p$ ), packing, container or canister (in J/m<sup>3</sup>/K)  
- Variables *rhoCpr, rhoCpp, rhoCpc*
- 11 Initial temperature ( in °C Celsius) and vertical extent of repository (in meters)  
- Variables *tzero, vert*

For the baseline case, this block of data is listed as follows:

- Line No.
- 6 Temperature Parameters
- 7 4.44473e8 ! initial power density in J/yr/m<sup>2</sup>
- 8 70000., 2.3, 10. ! metric ton initial heavy metal total, MTIHM can, age of fuel
- 9 5.68e7, 3.787e7, 3.26e6 ! J/yr/m/K thermal conductivity for rock, packing, can
- 10 2.4e6, 1.2e6, 1.2e6 ! rho\*Cp (volumetric heat capacity of rock) in J/m<sup>3</sup>/K, rock, packing, can
- 11 23., 4.0 ! initial temperature and vertical extent of repository

### 4.4 ENVIRONMENTAL MODEL INPUT

The third block of data describes the environmental model as follows:

- Line No.
- 12 Title line for environmental model input
- 13 Diffusive coefficient (D) of water vapor in air (in m<sup>2</sup>/yr), reference temperature (in °C Celsius), tortuosity factor ( $\tau$ ) for rock and packing  
- Variables *d, tdiff, taur, taup*
- 14 Porosity for rock ( $\phi$ ), porosity for packing, liquid water film thickness formed on the surface of container  
- Variables *phir, phip, delta* (in m)

- 15 The number of time and drip rate pairs  
- Variable *ndrip*
- 16 Time in years, drip rate (in m/yr)  
- Variables *qtime(i), qdrip(i)*
- 17 Time in years, drip rate (in m/yr)  
- Variables *qtime(i), qdrip(i)*
- 18 Time in years, drip rate (in m/yr)  
-Variables *qtime(i), qdrip(i)*
- 19 Time in years, drip rate (in m/yr)  
-Variables *qtime(i), qdrip(i)*
- 20 Time in years, drip rate (in m/yr)  
-Variables *qtime(i), qdrip(i)*
- 21 Time in years, drip rate (in m/yr)  
-Variables *qtime(i), qdrip(i)*
- 22 Salt (in Kg/m<sup>3</sup>), scale (in Kg/m<sup>3</sup>)  
-Variables *salt, scale*
- 23 Scale factor for vapor pressure lowering relative to NaCl solution  
-Variable *bfact*
- 24 Initial salt amount (in Kg), initial scale amount (in Kg)  
-Variables *dsalt, dscale*
- 25 Model selection (0=> no umbrella, 1=> umbrella effect), funnel area for capture of Darcy flow onto container (in m<sup>2</sup>)  
-Variables *idrip, dfrac*
- 26 Umbrella edge thickness (in m), umbrella edge temperature (in °C Celsius), range of temperature (in °C Celsius)  
-Variables *slice, tenhan, tslop*
- 27 Atmospheric pressure at Yucca Mt. repository level (in atm)  
-Variable *pref*

For the baseline case, this block of data is listed as follows:

Line

No.

- 12 Evaporation Parameters
- 13 962., 59., 1.0, 1.0 !diffusive coef. (m<sup>2</sup>/yr), reference temp. (°C), tortuosity for rock and packing
- 14 0.12, 0.12, 2.e-3 ! porosity for rock, porosity for packing, water film thick (m)
- 15 6 ! ndrip, the number of time, drip rate pairs
- 16 0., 1.e-3 ! time in yr, drip rate in m/yr
- 17 100., 1.e-3 ! time in yr, drip rate in m/yr
- 18 400., 1.e-3 ! time in yr, drip rate in m/yr
- 19 3000., 1.e-3 ! time in yr, drip rate in m/yr
- 20 8000., 1.e-3 ! time in yr, drip rate in m/yr
- 21 100000., 1.e-3 ! time in yr, drip rate in m/yr
- 22 0.0613, 0.2121 ! salt (Kg/m<sup>3</sup>), scale (Kg/m<sup>3</sup>)
- 23 1.0 ! bfact, scale factor for vapor pressure lowering relative to NaCl solution
- 24 0.1, 0.0 ! initial salt (Kg), initial scale (Kg)
- 25 1, 1.0 ! idrip (0=> no umbrella, 1=> umbrella effect), qfrac in m<sup>2</sup> (fraction of Darcy flux)

- 26 20., 95, 2. ! umbrella edge thickness (m), umbrella edge temp. (°C), range of temp. (°C)
- 27 0.895 ! atmospheric pressure (atm)

#### 4.5 RELEASE RATE AND SOLVER PARAMETERS INPUT

The fourth block of data describes the release rate and solver parameters as follows:

- Line No.
- 28 Spent fuel alteration rate/yr (alt), radioactive decay rate/yr ( $\lambda$ )  
-Variables *alt, rlam*
  - 29 Initial time step (in yr), max time step (in yr), constant for selecting solver  
0->full equilibrium (Lsode), 1-> local equilibrium (ODE)  
Variables *dtini, dtmax, isolve*
  - 30 Relative error, absolute error for Lsode solver  
-Variables *errel, errabs*  
Variables not used but will be enhanced later)
  - 31 Evap/Qin factor (variable for future enhancement), fraction of maximum surface water coverage before full evaporation occurs (below this amount, local equilibrium is assumed)  
-Variables *junk, amtund*

For the baseline case, this block of data is listed as follows:

- Line No.
- 28 1.e-3, 1.39e-4 ! alt, lambda (release rate parameters)
  - 29 1.e-3, 1.e0, 1 ! initial time step, max time step, 0->full (Lsode), 1-> local equilibrium
  - 30 1.e-3, 1.e-3 ! relative error, absolute error (Lsode)
  - 31 10., 0.01 ! Evap/Qin factor, Vwater/Vcrit factor to switch from local equilibrium

#### 4.6 CORROSION MODEL INPUT

The fifth block of data describes the corrosion model as follows:

- Line No.
- 32 Title line for corrosion model
  - 33 Beta kinetics parameter for oxygen ( $\beta_{O_2}$ ) and water reduction reactions ( $\beta_{H_2O}$ )  
-Variables *betaox, betahy*
  - 34 Rate constant for oxygen and water reduction reactions ( $k_{H_2O}$ ) (all in (C m)/(mole yr)), activation energy for oxygen and water rate constant (J/mole)  
-Variables *rkox, rkhy, gox, ghy*
  - 35 Current density for air/steam, active current density (all in C/m<sup>2</sup>/yr)  
-Variables *curair, curact*
  - 36 Passive current density (in C/m<sup>2</sup>/yr), temperature constant for first-order, temperature constant for second-order  
-Variables *aa(1), aa(2), aa(3)*

- 37 Linear interpolation factor for using passive or active current density [0 (passive)-1 (active)], constants for future enhancement  
-Variables *bb(1), bb(2), bb(3), bb(4), bb(5), bb(6)*
- 38 Nitrate/chloride ratio, reference pH  
-Variables *clrat, refph*
- 39 Tortuosity in scale, scale porosity ( $\phi$ )  
-Variables *taus, spor*

For the baseline case, this block of data is listed as follows:

Line

No.

- 32 Corrosion Parameters
- 33 0.75, 0.5 ! beta kinetics parameter for oxygen and water
- 34 3.e10, 3.2, 100000., 20000. ! rate constant for oxygen and water reduction, Gox, Ghy
- 35 6.3e2, 6.3e6 ! current density for air/steam, active current density
- 36 6.3e4, 0.0, 0.0 ! passive current density, const., const.
- 37 0.0, 0.0, 0.0, 0.0, 0.0, 0.0 ! CEcrit,Counter,const.,const.,const.,const.
- 38 1.0, 7.0 ! nitrate/cl ratio, reference pH
- 39 0.3, 0.5 ! tortuosity in scale, scale porosity

#### 4.7 MECHANICAL MODEL INPUT

The mechanical properties of the alloys, which include yield strength (MPa), Young's modulus (MPa), Poisson's ratio, and Fracture Toughness (MPa•m<sup>1/2</sup>), are required by the SCCEX code. These mechanical properties will be used to compute the residual strengths (discussed in Section 2.6) that can be compared with a deterministic seismic-induced stress to determine if a mechanical failure occurs. All these mechanical properties are currently hard-coded in the SCCEX code; however, it is not very convenient when different materials are used. To enhance the SCCEX code, these material properties data should also be included in the current SCCEX code input file.

As discussed in the report (Cragolino et al., 1994), five different materials were used to validate different failure mechanisms defined in the SCCEX code. Among these materials, 304L SS and alloy 825 are existing materials, and material X, material Y, and material Z are hypothetical materials. In this manual, 304L SS is the standard material which has yield strength of 170 MPa, Young's modulus of 1.82•10<sup>5</sup> MPa, Poisson's ratio of 0.25, and fracture toughness of 300 MPa•m<sup>1/2</sup>. The rest of the material properties can be seen in the report (Cragolino et al., 1994).

The mechanical properties at the temperature of interest were considered to be equal to those at room temperature (20 °C) multiplied by temperature-dependent functions. For 304L SS material, several temperature-dependent functions were calculated and listed in Table 4-1. No temperature correction was applied to fracture toughness. When using other materials, these temperature-dependent functions must also be developed.

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Table 4-1. Temperature corrections for mechanical properties

Properties at Temperature $T =$ (Properties at 20 °C) $\times f(T)$	Temperature Function, $f(T)$ $T: \text{°C}$
Yield Strength (MPa)	$1-10^{-3} (T-20)$
Young's Modulus (MPa)	$1-6\times 10^{-4} (T-20)$
Poisson's ratio	$1+4\times 10^{-4} (T-20)$

## 5 DESCRIPTION OF OUTPUT FILES

### 5.1 OVERVIEW

The output files for this code include the following: sccsml.dat, mechanical.out, simple.out, main.out, summary.out, and release.out. These files are used to record the key solutions for validation, plotting, and postprocessing purposes. In the following subsections, the main purpose of each output file is discussed briefly, and a demonstration output file based on the baseline input is also included.

### 5.2 SCCSML.DAT

The file sccsml.dat (see Table 5-1) summarizes the weight factor, failure time, time-to-wetting, and time to leach for all calculation cells. For the later probabilistic analysis (not described here), where SCCEX code will be called several times, the results of every sccsml.dat file will be stored and will be analyzed by a postprocess code.

Table 5-1. Output file — SCCSML.DAT

***** SCCEX FAILURE, WETTING, LEACHATE TIME *****	
1	! total calculation groups
1	! counter
4	! weight factor
785.00	4 ! failure time, type (0: No failure, 1: Buckling, 2: Fracture, 3: Yield, 4: Corrosion)
735.00	1 ! wetting time, type (0: no wet, 1: wet)
1000.00	0 ! leachate time, type (0: no leachate, 1: leachate)

Note that explanations after the exclamation point are added to explain the results and will not be seen in the original output file. The same format is used for the other subsections.

### 5.3 MECHANICAL.OUT

The file mechanical.out (see Table 5-2) summarizes the temperature, wetted area, remaining thickness of the container, and leachate in each time step. This file will be read by one of the SCCEX code subroutines (mechanical) to determine if the container fails or not.

Table 5-2. Output file — MECHANICAL.OUT

1	4	101	1	! Counter, weight factor, total time steps, calculation cells	
1	0.100E-02	0.145E+03	0.100E-01	0.000E+00	0.000E+00
!(time step, years, temperature, remaining thickness, wetted area, leachate)					
2	0.100E+02	0.154E+03	0.100E-01	0.000E+00	0.000E+00
3	0.200E+02	0.155E+03	0.100E-01	0.000E+00	0.000E+00
4	0.300E+02	0.152E+03	0.100E-01	0.000E+00	0.000E+00
5	0.400E+02	0.148E+03	0.100E-01	0.000E+00	0.000E+00
6	0.500E+02	0.143E+03	0.100E-01	0.000E+00	0.000E+00
7	0.600E+02	0.139E+03	0.100E-01	0.000E+00	0.000E+00
8	0.700E+02	0.135E+03	0.100E-01	0.000E+00	0.000E+00

**Table 5-2. Output file — MECHANICAL.OUT (Cont'd)**

9	0.800E+02	0.132E+03	0.100E-01	0.000E+00	0.000E+00
10	0.900E+02	0.128E+03	0.100E-01	0.000E+00	0.000E+00
11	0.100E+03	0.126E+03	0.100E-01	0.000E+00	0.000E+00
12	0.110E+03	0.124E+03	0.100E-01	0.000E+00	0.000E+00
13	0.120E+03	0.122E+03	0.100E-01	0.000E+00	0.000E+00
14	0.130E+03	0.120E+03	0.100E-01	0.000E+00	0.000E+00
15	0.140E+03	0.119E+03	0.100E-01	0.000E+00	0.000E+00
16	0.150E+03	0.117E+03	0.100E-01	0.000E+00	0.000E+00
*					
* 17-95 or 160-940 years data					
*					
96	0.950E+03	0.927E+02	-0.413E-04	0.676E+01	0.000E+00
97	0.960E+03	0.925E+02	-0.416E-04	0.730E+01	0.000E+00
98	0.970E+03	0.924E+02	-0.418E-04	0.641E+01	0.000E+00
99	0.980E+03	0.922E+02	-0.420E-04	0.659E+01	0.000E+00
100	0.990E+03	0.921E+02	-0.423E-04	0.685E+01	0.000E+00
101	0.100E+04	0.919E+02	-0.425E-04	0.718E+01	0.000E+00

## 5.4 SIMPLE.OUT

The file simple.out (see Table 5-3) is an output file designed for plotting purposes. Data of several important parameters, which include the temperature at canister surface, vapor pressure, and evaporation rate, can be plotted as a function of time.

**Table 5-3. Output File — SIMPLE.OUT**

time, tcan(i), tout(i), tcan(i)-tout(i), vpin, vout, vpin*.75, erate (m <sup>3</sup> /y), e(m <sup>3</sup> /m <sup>2</sup> /y)									
! (time, canister surface temp., outer temp., temp. diff., vapor pressure inside, vapor pressure outside, 0.75*vapin, evaporation rate, evaporation rate)									
0.00E+00	1.45E+02	2.30E+01	1.22E+02	4.23E+00	4.19E-02	3.18E+00	1.00E+00	1.01E-01	
1.00E+01	1.54E+02	5.97E+01	9.43E+01	5.33E+00	1.94E-01	4.00E+00	1.00E+00	1.01E-01	
2.00E+01	1.55E+02	7.61E+01	7.86E+01	5.41E+00	3.98E-01	4.06E+00	1.00E+00	1.01E-01	
3.00E+01	1.52E+02	8.51E+01	6.67E+01	5.06E+00	5.74E-01	3.79E+00	1.00E+00	1.01E-01	
4.00E+01	1.48E+02	9.05E+01	5.73E+01	4.54E+00	7.06E-01	3.41E+00	1.00E+00	1.01E-01	
5.00E+01	1.43E+02	9.37E+01	4.98E+01	3.99E+00	7.96E-01	2.99E+00	1.00E+00	1.01E-01	
6.00E+01	1.39E+02	9.55E+01	4.37E+01	3.44E+00	8.51E-01	2.58E+00	1.00E+00	1.01E-01	
7.00E+01	1.35E+02	9.65E+01	3.87E+01	2.94E+00	8.81E-01	2.20E+00	1.00E+00	1.01E-01	
8.00E+01	1.32E+02	9.69E+01	3.48E+01	2.48E+00	8.94E-01	1.86E+00	1.00E+00	1.01E-01	
9.00E+01	1.28E+02	9.70E+01	3.15E+01	2.22E+00	8.96E-01	1.67E+00	1.00E+00	1.01E-01	
1.00E+02	1.26E+02	9.69E+01	2.91E+01	2.15E+00	8.93E-01	1.61E+00	1.00E+00	1.01E-01	
1.10E+02	1.24E+02	9.67E+01	2.71E+01	2.08E+00	8.88E-01	1.56E+00	1.00E+00	1.01E-01	
1.20E+02	1.22E+02	9.65E+01	2.54E+01	2.02E+00	8.81E-01	1.51E+00	1.00E+00	1.01E-01	
1.30E+02	1.20E+02	9.63E+01	2.39E+01	1.96E+00	8.73E-01	1.47E+00	1.00E+00	1.01E-01	

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**Table 5-3. Output File — SIMPLE.OUT (Cont'd)**

1.40E+02	1.19E+02	9.60E+01	2.26E+01	1.88E+00	8.64E-01	1.41E+00	1.00E+00	1.01E-01
1.50E+02	1.17E+02	9.57E+01	2.14E+01	1.80E+00	8.55E-01	1.35E+00	1.00E+00	1.01E-01
*								
* 160-940 years data								
*								
9.50E+02	9.27E+01	8.63E+01	6.36E+00	7.65E-01	6.03E-01	5.73E-01	7.17E-01	7.27E-02
9.60E+02	9.25E+01	8.62E+01	6.31E+00	7.60E-01	6.00E-01	5.70E-01	6.97E-01	7.06E-02
9.70E+02	9.24E+01	8.61E+01	6.26E+00	7.56E-01	5.98E-01	5.67E-01	6.77E-01	6.86E-02
9.80E+02	9.22E+01	8.60E+01	6.21E+00	7.52E-01	5.96E-01	5.64E-01	6.58E-01	6.67E-02
9.90E+02	9.21E+01	8.59E+01	6.16E+00	7.48E-01	5.93E-01	5.61E-01	6.40E-01	6.49E-02
1.00E+03	9.19E+01	8.58E+01	6.11E+00	7.44E-01	5.91E-01	5.58E-01	6.21E-01	6.30E-02

### 5.5 MAIN.OUT

The file main.out (see Table 5-4) is an output file designed for plotting purposes. Data of several important parameters, which include the volume of water, kg of NaCl, corrosion depth, effluent drip rate, and drip rate, etc., can be plotted as a function of time.

**Table 5-4. Output File — MAIN.OUT**

time,	Vwater,	KgNaCl,	depth,	Qout,	Kg scale,	%NaCl,	corr rate,	Ecorr,	Tcan,	Qin
!(time,	volume of water,	Kg of NaCl,	corrosion depth,	effluent drip rate,	Kg of scale,	NaCl percent,	corrosion rate,	Corrosion potential,	canister surface temp.,	drip rate)
1.00E-03	0.00E+00	1.00E-01	2.40E-11	0.00E+00	0.00E+00	2.75E+01	2.40E-08	-9.00E+00		
1.45E+02	0.00E+00									
1.00E+01	0.00E+00	1.00E-01	2.40E-07	0.00E+00	0.00E+00	2.75E+01	2.40E-08	-9.00E+00		
1.54E+02	0.00E+00									
2.00E+01	0.00E+00	1.00E-01	4.79E-07	0.00E+00	0.00E+00	2.75E+01	2.40E-08	-9.00E+00		
1.55E+02	0.00E+00									
3.00E+01	0.00E+00	1.00E-01	7.19E-07	0.00E+00	0.00E+00	2.75E+01	2.40E-08	-9.00E+00		
1.52E+02	0.00E+00									
4.00E+01	0.00E+00	1.00E-01	9.59E-07	0.00E+00	0.00E+00	2.75E+01	2.40E-08	-9.00E+00		
1.48E+02	0.00E+00									
5.00E+01	0.00E+00	1.00E-01	1.20E-06	0.00E+00	0.00E+00	2.75E+01	2.40E-08	-9.00E+00		
1.43E+02	0.00E+00									
6.00E+01	0.00E+00	1.00E-01	1.44E-06	0.00E+00	0.00E+00	2.75E+01	2.40E-08	-9.00E+00		
1.39E+02	0.00E+00									
7.00E+01	0.00E+00	1.00E-01	1.68E-06	0.00E+00	0.00E+00	2.75E+01	2.40E-08	-9.00E+00		
1.35E+02	0.00E+00									
8.00E+01	0.00E+00	1.00E-01	1.92E-06	0.00E+00	0.00E+00	2.75E+01	2.40E-08	-9.00E+00		
1.32E+02	0.00E+00									
9.00E+01	0.00E+00	1.00E-01	2.16E-06	0.00E+00	0.00E+00	2.75E+01	2.40E-08	-9.00E+00		
1.28E+02	0.00E+00									
1.00E+02	0.00E+00	1.00E-01	2.40E-06	0.00E+00	0.00E+00	2.75E+01	2.40E-08	-9.00E+00		
1.26E+02	0.00E+00									
1.10E+02	0.00E+00	3.23E-01	2.64E-06	0.00E+00	7.71E-01	2.75E+01	2.40E-08	-9.00E+00		
1.24E+02	4.04E-01									

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Table 5-4. Output File — MAIN.OUT (Cont'd)

1.20E+02	0.00E+00	5.71E-01	2.88E-06	0.00E+00	1.63E+00	2.75E+01	2.40E-08	-9.00E+00
1.22E+02	4.04E-01							
1.30E+02	0.00E+00	8.18E-01	3.12E-06	0.00E+00	2.49E+00	2.75E+01	2.40E-08	-9.00E+00
1.20E+02	4.04E-01							
1.40E+02	0.00E+00	1.07E+00	3.36E-06	0.00E+00	3.34E+00	2.75E+01	2.40E-08	-9.00E+00
1.19E+02	4.04E-01							
1.50E+02	0.00E+00	1.31E+00	3.59E-06	0.00E+00	4.20E+00	2.75E+01	2.40E-08	-9.00E+00
1.17E+02	4.04E-01							
*								
* 160-940 years data								
*								
9.50E+02	1.35E-02	4.00E+00	1.00E-02	0.00E+00	1.35E+01	2.28E+01	2.40E-08	-9.00E+00
9.27E+01	1.00E-03							
9.60E+02	1.46E-02	4.00E+00	1.00E-02	0.00E+00	1.35E+01	2.15E+01	2.40E-08	-9.00E+00
9.25E+01	1.00E-03							
9.70E+02	1.28E-02	4.01E+00	1.00E-02	0.00E+00	1.35E+01	2.38E+01	2.40E-08	-9.00E+00
9.24E+01	1.00E-03							
9.80E+02	1.32E-02	4.01E+00	1.00E-02	0.00E+00	1.35E+01	2.33E+01	2.40E-08	-9.00E+00
9.22E+01	1.00E-03							
9.90E+02	1.37E-02	4.01E+00	1.00E-02	0.00E+00	1.35E+01	2.26E+01	2.40E-08	-9.00E+00
9.21E+01	1.00E-03							
1.00E+03	1.44E-02	4.01E+00	1.00E-02	0.00E+00	1.35E+01	2.18E+01	2.40E-08	-9.00E+00
9.19E+01	1.00E-03							

### 5.6 SUMMARY.OUT

The file summary.out (see Table 5-5) summarizes some of the main results, which are similar to those in file sccsml.dat.

Table 5-5. Output File — SUMMARY.OUT

1	101	4	!calculation cell, points/cell, total cells					
4	0.571E+03	0.571E+03	0.731E+03	0.963E+02	0.100E+04	0.000E+00	0.790E+03	
! (Weight factor, x axis position, y axis position, time of first wetting, temp. at first wetting, time of effluent generation, temp. at first effluent, time to fail)								

### 5.7 RELEASE.OUT

The file release.out (see Table 5-6) summarizes radionuclide release information. Data of this file can be plotted as a function of time to study the effect of input parameters.

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Table 5-6. Output File — RELEASE.OUT

! time step, fractional radionuclide release /yr, proportion of initial inventory in waste, proportion of initial inventory in waste package water, proportion of initial inventory in waste released from wp, radionuclide output

1.00E-04	0.00E+00	1.00E+00	0.00E+00	0.00E+00	0.00E+00
1.00E+01	0.00E+00	9.99E-01	0.00E+00	0.00E+00	0.00E+00
2.00E+01	0.00E+00	9.97E-01	0.00E+00	0.00E+00	0.00E+00
3.00E+01	0.00E+00	9.96E-01	0.00E+00	0.00E+00	0.00E+00
4.00E+01	0.00E+00	9.94E-01	0.00E+00	0.00E+00	0.00E+00
5.00E+01	0.00E+00	9.93E-01	0.00E+00	0.00E+00	0.00E+00
6.00E+01	0.00E+00	9.92E-01	0.00E+00	0.00E+00	0.00E+00
7.00E+01	0.00E+00	9.90E-01	0.00E+00	0.00E+00	0.00E+00
8.00E+01	0.00E+00	9.89E-01	0.00E+00	0.00E+00	0.00E+00
9.00E+01	0.00E+00	9.88E-01	0.00E+00	0.00E+00	0.00E+00
1.00E+02	0.00E+00	9.86E-01	0.00E+00	0.00E+00	0.00E+00
1.10E+02	0.00E+00	9.85E-01	0.00E+00	0.00E+00	0.00E+00
1.20E+02	0.00E+00	9.83E-01	0.00E+00	0.00E+00	0.00E+00
1.30E+02	0.00E+00	9.82E-01	0.00E+00	0.00E+00	0.00E+00
1.40E+02	0.00E+00	9.81E-01	0.00E+00	0.00E+00	0.00E+00
1.50E+02	0.00E+00	9.79E-01	0.00E+00	0.00E+00	0.00E+00
*					
* 160-940 years data					
*					
9.50E+02	0.00E+00	7.36E-01	1.41E-01	0.00E+00	0.00E+00
9.60E+02	0.00E+00	7.26E-01	1.49E-01	0.00E+00	0.00E+00
9.70E+02	0.00E+00	7.16E-01	1.58E-01	0.00E+00	0.00E+00
9.80E+02	0.00E+00	7.06E-01	1.66E-01	0.00E+00	0.00E+00
9.90E+02	0.00E+00	6.97E-01	1.75E-01	0.00E+00	0.00E+00
1.00E+03	0.00E+00	6.87E-01	1.83E-01	0.00E+00	0.00E+00

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## 6 CONCLUSION

The SCCEX Computer code has been developed to demonstrate an approach for evaluating containment by a waste package and to identify those areas requiring more detailed analysis. This report presents a brief theory description of several models used in the SCCEX code. These models include the repository thermal fields, near-field environment, corrosion of container materials, and mechanical failure models. The SCCEX code structure, capability, compilation and linking, hardware requirements and installation procedure, and user support were also discussed. In addition, the baseline case input data requirements and the corresponding output files were presented. The results of this computer code were used in support of evaluating the substantially complete containment rule for waste packages in 10 CFR Part 60 (Cragolino et al., 1994).

To implement the SCCEX code, however, the simplified nature of the models and the assumptions and approximations were made to provide a quantitative representation of the actual conditions that may be presented in an unsaturated repository site as the one modeled here. For example, a simplified thermal model was adopted to facilitate the parametric calculations. However, it has limitations arising from the effect of the outer distance,  $r_3$ , on the calculated value of  $\Delta T$  and the fact that  $\Delta T$  is assumed to be independent of the spacing between containers. Another shortcoming is that the current SCCEX code does not consider the chemistry of the final solution more rigorously [e.g., inhibiting species for localized corrosion (i.e., nitrate) as well as other anions, such as sulfate, bicarbonate, etc]. Other limitations are discussed in the report by Cragolino et al. (1994).

The current SCCEX code is applicable to various kinds of designs that involve different materials and failure mechanisms (Cragolino et al., 1994). In addition, the code can be used to study the sensitivity of the input parameters and can be coupled with probabilistic analysis methods to determine if the container is "substantially complete containment" (Cragolino et al., 1994). The SCCEX code has provided an initial step to explore the complex problem of HLW waste containment.

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