

*FEHMN 1.0: Finite Element Heat  
and Mass Transfer Code*

HYDROLOGY DOCUMENT NUMBER 709

**Los Alamos**

*Los Alamos National Laboratory is operated by the University of California for  
the United States Department of Energy under contract W-7405-ENG-36.*

*Prepared by Kay Coen, Group EES-5*

*This work was supported by the US Department of Energy,  
Yucca Mountain Site Characterization Project Office as part  
of the Civilian Radioactive Waste Management Program.*

*An Affirmative Action/Equal Opportunity Employer*

*This report was prepared as an account of work sponsored by an agency of the United States Government. Neither The Regents of the University of California, the United States Government nor any agency thereof, nor any of their employees, makes any warranty, express or implied, or assumes any legal liability or responsibility for the accuracy, completeness, or usefulness of any information, apparatus, product, or process disclosed, or represents that its use would not infringe privately owned rights. Reference herein to any specific commercial product, process, or service by trade name, trademark, manufacturer, or otherwise, does not necessarily constitute or imply its endorsement, recommendation, or favoring by The Regents of the University of California, the United States Government, or any agency thereof. The views and opinions of authors expressed herein do not necessarily state or reflect those of The Regents of the University of California, the United States Government, or any agency thereof.*

*FEHMN 1.0: Finite Element Heat  
and Mass Transfer Code*

*George Zyvoloski*

*Zora Dash*

*Sharad Kelkar*

## Contents

FIGURES . . . . .	vi
TABLES . . . . .	vii
ABSTRACT . . . . .	1
I. MODEL DESCRIPTION . . . . .	1
A. Nature and Purpose . . . . .	1
B. Mathematical Formulation . . . . .	2
C. Discretization of the Governing Equations . . . . .	14
D. Boundary Conditions . . . . .	17
E. Solution Methods . . . . .	17
F. Dual Porosity Formulation . . . . .	21
II. CODE DESCRIPTION . . . . .	25
A. Subroutines . . . . .	25
B. Common Block and Parameter Statements . . . . .	33
C. Subroutine Structure for FEHMN . . . . .	47
III. USER'S MANUAL . . . . .	51
A. Automatic Mesh Generation . . . . .	51
B. Macro Command Input for FEHMN . . . . .	56
C. Graphics Postprocessing . . . . .	76
D. Example Input Files and Output Files . . . . .	80
ACKNOWLEDGMENTS . . . . .	111
DISCLAIMER . . . . .	111
REFERENCES . . . . .	111

## FIGURES

1. Comparison of nodal connections for conventional and Lobatto integrations. . . .	16
2. Matrix band structures showing second-order fill-in. x - original matrix positions. o - fill-in with order 2 factorization. . . . .	20
3. Computational volume element showing dual porosity parameters . . . . .	22
4. Structure for subroutine calls for FEHMN. . . . .	48
5. Elements available with FEHMN in 2-D and 3-D problems showing numbering convention. . . . .	52
6. Nodal ordering for defining 2-D and 3-D domain blocks for GENMSH Input. . . .	53
7. Terminal output for a FEHMN run on a CRAY computer. . . . .	59
8. Schematic diagram of the 3-D heat conduction problem. . . . .	84
9. Input for preprocessor GENMESH for 3-D heat conduction example. . . . .	84
10. Grid for 4 x 4 x 4 heat conduction problem. . . . .	85
11. Input file for FEHMN for 3-D heat conduction example. . . . .	86
12. Computer output for the 3-D heat conduction example. . . . .	90
13. Instruction file (HIS.INS) for postprocessor FEHPLTR for the heat conduction problem. . . . .	92
14. History plot for the heat conduction problem. . . . .	93
15. Solution domain and results for the Toronyi example. . . . .	94
16. Input for GENMSH for the Toronyi example. . . . .	94
17. Input file for FEHMN for Toronyi example. . . . .	95
18. Output for the Toronyi example. . . . .	98
19. Schematic diagram of the geometry and boundary conditions for the DOE code comparison project problem. . . . .	100
20. Comparison of FEHMN production well temperatures with results from other codes. . . . .	100
21. Comparison of FEHMN production well pressure with results from other codes.	101
22. Comparison of FEHMN observation well pressure with results from other codes.	101
23. Input for GENMSH for the DOE example. . . . .	102
24. Input for FEHMN for the DOE example. . . . .	102
25. Output from FEHMN for the DOE example. . . . .	108
26. Instruction file (CON.INS) for the postprocessor FECPLTR for the DOE problem. . . . .	109
27. Contour plot of temperature for the DOE problem. . . . .	110

## TABLES

I. Notation . . . . .	3
II. Sorption Isotherm Models . . . . .	10
III. Subroutine Calls Within FEHMN . . . . .	25
IV. Capabilities of FEHMN with Macro Command References . . . . .	57
V. FEHMN Files . . . . .	57
VI. Macro Control Statements for FEHMN . . . . .	60
VII. Input Description for FEHMN . . . . .	62
VIII. Input Parameters for the 3-D Heat Conduction Problem . . . . .	80
IX. Sample Problems for 3-D Heat Conduction . . . . .	81
X. Comparison of Analytical and Model Results for 3-D Heat Conduction . . . . .	81
XI. Input Parameters for Toronyi Example . . . . .	82
XII. Input Parameters for the DOE Code Comparison Project . . . . .	83

**FEHMN 1.0:  
FINITE ELEMENT HEAT AND MASS TRANSFER CODE**

by

George Zyvoloski, Zora Dash, and Sharad Kelkar

**ABSTRACT**

A computer code is described which can simulate non-isothermal multi-phase multicomponent flow in porous media. It is applicable to natural-state studies of geothermal systems and ground-water flow. The equations of heat and mass transfer for multiphase flow in porous and permeable media are solved using the finite element method. The permeability and porosity of the medium are allowed to depend on pressure and temperature. The code also has provisions for movable air and water phases and noncoupled tracers; that is, tracer solutions that do not affect the heat and mass transfer solutions. The tracers can be passive or reactive. The code can simulate two-dimensional, two-dimensional radial, or three-dimensional geometries. A summary of the equations in the model and the numerical solution procedure are provided in this report. A user's guide and sample problems are also included.

---

## **I. MODEL DESCRIPTION**

### **A. Nature and Purpose**

The FEHMN (Finite Element Heat and Mass Nuclear) code, described in this report, is a version of FEHM (Finite Element Heat and Mass, Zyvoloski et al., 1988) developed for the Yucca Mountain Site Characterization Project (YMP) and documented as required by NUREG-0856. This report satisfies the document requirements for model description and user's manual as presented in the LANL YMP Computer Software Control Quality Procedure (SQAP-3.7, R0). The verification and validation reports are produced as separate documents. The main use of FEHMN will be to assist in the understanding of flow fields in the saturated zone below the potential Yucca Mountain repository. This is referred to as the C-Wells project (YMP-LANL-SP-8.3.1.2.3.1.7). Also in regards to that project, the code will be used to design tracer tests (reactive and non-reactive) to characterize the flow field below Yucca Mountain. In addition, FEHMN will be used to study coupled processes (multicomponent and natural convection) in the unsaturated zone (YMP-LANL-SCP-8.3.1.3.7.1). We note here that the model requirements may be found in the above mentioned study plans.

Yucca Mountain is extremely complex both hydrologically and geologically. The computer codes that are used to model flow must be able to describe that complexity. For example, the flow at Yucca Mountain, in both the saturated and unsaturated zones is dominated by fracture and fault flow in many areas. With permeation to and from faults and fractures, the flow is inherently three-dimensional (3-D). Birdsell et al. (1990) recently presented calculations showing the importance of 3-D flow at Yucca Mountain. Coupled heat and mass transport occurs in both the unsaturated and saturated zones. In the far field unsaturated zone, Weeks (1987) has described natural convection that occurs through Yucca Mountain due to seasonal temperature changes. Heat and mass transfer are important in the saturated zone modeling of temperature logs and pressure tests.

The governing equations and solution techniques used in the FEHMN code are described below. In addition, a user's manual with example problems is provided. Future changes to the code and documentation will be made in accordance with quality assurance procedures being established for the Yucca Mountain Site Characterization Project.

## B. Mathematical Formulation

**1. Governing equations.** Detailed derivations of the governing equations for two-phase flow including heat transfer have been presented by several investigators (Mercer and Faust, 1975, and Brownell et al., 1975, for example), and therefore only a brief development will be presented here. The notation used in this report is given in Table I.

Conservation of mass is expressed by the equation

$$\frac{\partial A_m}{\partial t} + \nabla \cdot \bar{f}_m + q_m = 0 \quad , \quad (1)$$

where the mass per unit volume,  $A_m$ , is given by

$$A_m = \phi(S_v \rho_v + S_\ell \rho_\ell) \quad (2)$$

and the mass flux,  $\bar{f}_m$ , is given by

$$\bar{f}_m = \rho_v \bar{V}_v + \rho_\ell \bar{V}_\ell \quad . \quad (3)$$

Here  $\phi$  is the porosity of the matrix,  $S_v$  and  $S_\ell$  are saturations,  $\rho_v$  and  $\rho_\ell$  are densities, and  $\bar{V}_v$  and  $\bar{V}_\ell$  are velocities with the subscripts  $v$  and  $\ell$  indicating quantities for the vapor phase and the liquid phase, respectively. Source and sink terms (such as bores, reinjection wells, or groundwater recharge) are represented by the term  $q_m$ .

Conservation of fluid-rock energy is expressed by the equation

$$\frac{\partial A_e}{\partial t} + \nabla \cdot \bar{f}_e + q_e = 0 \quad . \quad (4)$$



---



---

**TABLE I. Notation**


---

$A$	parameter used in nonlinear adsorption model (Freundlich, modified Freundlich)
$[A]$	solution matrix for system of nonlinear equations
$A_c$	accumulation term for tracer ( $M/L^3$ )
$A_e$	energy accumulation term ( $M/L^2$ )
$A_m$	mass accumulation term ( $M/L^3$ )
$\tilde{[A]}$	approximation of matrix $[A]$
$a$	weighting factor for time discretization
$a_1, a_2, a_3, a_4$	coefficients used in reaction rate model
$\{b\}$	right hand side (forcing function) for system of linear equations
$C_l$	tracer concentration in liquid
$C_R$	tracer concentration adsorbed on rock
$C_v$	tracer concentration in vapor
$C_{max}$	parameter used in nonlinear adsorption model (modified Freundlich)
$[\tilde{C}]$	capacitance matrix
$C_{ij}^{up}$	upwind value of tracer concentration
$c_g$	parameter used in linear porosity model
$c_{pa}$	heat capacity of air $L^2/\theta^2 T$
$c_r$	parameter used in linear porosity model
$cp_1, cp_2$	parameters used in the capillary pressure models
$cp_3, cp_4$	parameters used in the capillary pressure models
$D_c$	dispersion coefficient for tracer ( $L^2/\theta$ )
$[D_c]$	finite element coefficients for tracer dispersion term
$D_{el}$	energy transmissibility term for liquid ( $L^2/\theta$ )
$D_{e,v}$	energy transmissibility term for vapor ( $L^2/\theta$ )
$D_{ml}$	mass transmissibility term for liquid ( $\theta$ )
$D_{m,v}$	mass transmissibility term for vapor ( $\theta$ )
$D_e^{up}$	upwind energy transmissibility term ( $L^2/\theta$ )
$D_m^{up}$	upwind mass transmissibility term ( $\theta$ )
$\{e\}$	unit vector
$E$	Youngs modulus ( $ML/\theta^2$ )
$F$	function representation
$\ F\ $	$L^2$ norm of residuals
$[F_c]$	residual for tracer equation
$F_e$	flux vector for energy equation ( $M/\theta^3$ )
$F_m$	flux vector for mass equation ( $M/L^2$ )
$\overline{F}(\overline{x})$	vector of equation residuals
$\{F_e\}$	residual for energy equations
$\{F_m\}$	residual for mass equation
$f(y)$	intermediate calculation in GMRES acceleration
$g$	acceleration of gravity ( $L/\theta^2$ )
$[H]^m$	intermediate calculation in GMRES acceleration

---



---

**TABLE I. Notation**


---

$h$	generalized energy variable ( $T$ or $L^2/\theta^2$ )
$h_a$	enthalpy of air ( $L^2/\theta^2$ )
$h_m^{mel}$	parameter in GMRES acceleration
$h_v$	mass fraction of air in the vapor phase
$h_{v,w}$	vapor enthalpy ( $L^2/\theta^2$ )
$h_l$	mass fraction of air in the liquid phase
$h_{l,w}$	liquid enthalpy ( $L^2/\theta^2$ )
$I_i$	impedance at node $i$ ( $\theta/L^2$ )
$I_{e,i}$	heat flow impedance at node $i$ ( $M/L^3\theta T$ )
$[K]$	finite element coefficient for heat conduction term
$K_D$	retardation coefficient (linear adsorption)
$K_{h,v,w}$	thermal conductivity ( $ML/T\theta^3$ )
$k$	intrinsic rock permeability ( $L^2$ )
$L_f, L_0$	length scales used in dual porosity problem
$L_{f1}, L_{f2}$	length scales used in dual porosity problem
$[\tilde{L}]$	approximate lower factorization of matrix
$m$	exponent used in Gangi stress model
$[N]$	finite element shape function
$Q_m$	source term for mass equation ( $M/\theta L^3$ )
$q_c$	source term for tracer ( $M/\theta L^3$ )
$q_e$	source term for energy equation ( $M/L^3\theta$ )
$q_i$	mass source term at node $i$ ( $M/\theta L^3$ )
$q_{e,i}$	energy source term at node $i$ ( $M/L^3\theta$ )
$\{q_e\}$	coefficient for energy source terms
$\{q_m\}$	coefficient for mass source terms
$P_c$	closure stress for use in Gangi stress model ( $ML$ )
$P_o$	initial pressure ( $ML/\theta^2$ )
$P_l$	liquid pressure ( $M/L\theta^2$ )
$P_v$	vapor pressure ( $M/L\theta^2$ )
$P_{cap}$	capillary pressure ( $M/L\theta^2$ )
$P_{flow}$	flowing pressure at node $i$ ( $M/L\theta^2$ )
$[R_c]$	coefficients for tracer gravity term
$R_l$	liquid relative permeability
$\{R_e\}$	gravity term coefficient for energy
$\{R_m\}$	gravity term coefficient for mass

---



---

Table I. Notation

---



---

$R_v$	vapor relative permeability
$\{r\}$	residual of linear system of equations
$r, r_b$	parameters used in nonlinear adsorption model (Langmuir)
$r_{p1}, r_{p2}$	parameters used in relative permeability models
$r_{p3}, r_{p4}$	parameters used in relative permeability models
$S$	normalized liquid saturation
$S_\ell$	liquid saturation
$\hat{S}_\ell$	normalized liquid saturation
$S_{\ell r}$	residual liquid saturation
$S_{\ell s}$	maximum liquid saturation
$S_v$	vapor saturation
$T$	temperature ( $T$ )
$T^*$	absolute temperature ( $T$ )
$[T_e(P, h)]$	stiffness matrix for energy equation
$[T_c(C)]$	stiffness matrix for concentration equation
$[T_m(P, h)]$	stiffness matrix for mass equation
$T_{flow}$	flowing temperature at node $i$ ( $T$ )
$T_{ff}, T_{ff1}$	transfer terms in dual porosity solution
$T_{ff2}$	transfer terms in dual porosity solution
$t$	time ( $\theta$ )
$u_\ell$	liquid internal energy ( $L^2/\theta^2$ )
$u_v$	vapor internal energy ( $L^2/\theta^2$ )
$u_r$	rock internal energy ( $L^2/\theta^2$ )
$V_f$	volume fraction for fractures in a dual porosity problem
$V_{f0}, V_{f1}$	volume fractions used in a dual porosity problem
$V_{f2}$	volume fractions used in a dual porosity problem
$V_\ell$	liquid velocity ( $L/\theta$ )
$V_v$	vapor velocity ( $L/\theta$ )
$[V]^m$	intermediate calculation in GMRES acceleration
$[\hat{V}]$	approximate upper factorization of matrix
$\{v\}$	intermediate calculation of GMRES acceleration
$\{w\}$	parameter in GMRES acceleration
$\{y\}$	intermediate calculations in GMRES acceleration
$\bar{x}^i$	vector of corrections at iteration $i$
$\alpha$	coefficient of thermal expansion ( $1/T$ )
$\alpha_1, \alpha_2$	coefficients used in sorption models

---



---

Table I. Notation

---

$\varepsilon$	tolerance taken for solution scheme
$\lambda$	parameter used in defining the van Genutchen capillary pressure model
$\mu_a$	air viscosity ( $M/L\theta$ )
$\mu_\ell$	liquid phase viscosity ( $M/L\theta$ )
$\mu_{\ell,w}$	liquid water viscosity ( $M/L\theta$ )
$\mu_v$	vapor phase viscosity ( $M/L\theta$ )
$\mu_{v,w}$	steam viscosity ( $M/L\theta$ )
$\phi$	porosity
$\phi_o$	initial porosity
$\sigma$	fractional vapor flow parameter
$\sigma$	<i>in situ</i> stress ( $ML/\theta^2$ )
$\left(\frac{\partial \bar{F}}{\partial \bar{x}^k}\right)$	Jacobian matrix for nonlinear system

\* Units given in ML $\theta$ T system of dimensions:  
 Mass [M], length [L], time [ $\theta$ ], temperature [T]

---



---

where the energy per unit volume,  $A_e$ , is given by

$$A_e = (1 - \phi)\rho_r u_r + \phi(S_v \rho_v u_v + S_\ell \rho_\ell u_\ell) \quad (5)$$

and the energy flux,  $\bar{f}_e$ , is given by

$$\bar{f}_e = \rho_v h_v \bar{V}_v + \rho_\ell h_\ell \bar{V}_\ell - K \bar{\nabla} T \quad (6)$$

Here the subscript  $r$  refers to the rock matrix;  $u_r$ ,  $u_v$ , and  $u_\ell$  are specific internal energies;  $h_v$  and  $h_\ell$  are specific enthalpies;  $K$  is an effective thermal conductivity;  $T$  is the temperature; and  $q_e$  is the energy contributed from sources and sinks.

To complete the governing equations it is assumed that Darcy's Law applies to the movement of each phase:

$$\bar{V}_v = -\frac{kR_v}{\mu_v} (\bar{\nabla} p_v - \rho_v \bar{g}) \quad (7)$$

and

$$\bar{V}_\ell = -\frac{kR_\ell}{\mu_\ell} (\bar{\nabla} p_\ell - \rho_\ell \bar{g}) \quad (8)$$

Here  $k$  is the permeability,  $R_v$  and  $R_\ell$  are the relative permeabilities,  $\mu_v$  and  $\mu_\ell$  are viscosities,  $p_\ell$  and  $p_v$  the phase pressures, and  $g$  represents the acceleration due to gravity (the phase pressures are related by  $p_v = p_\ell + p_{cap}$ ). For simplicity, the equations are shown for an isotropic medium, though this restriction does not exist in the computer code.

Using Darcy's Law the basic conservation equations (1) and (4) can be rewritten

$$-\nabla \cdot (D_{m\ell} \nabla p_\ell) - \nabla \cdot (D_{mv} \nabla p_v) + q_m + \frac{\partial}{\partial z} g (D_{m\ell} \rho_\ell + D_{mv} \rho_v) + \frac{\partial A_m}{\partial t} = 0 \quad (9)$$

and

$$-\nabla \cdot (D_{e\ell} \nabla p_\ell) - \nabla \cdot (D_{ev} \nabla p_v) + \nabla \cdot (K \nabla T) + q_e + \frac{\partial}{\partial z} g (D_{e\ell} \rho_\ell + D_{ev} \rho_v) + \frac{\partial A_e}{\partial t} = 0, \quad (10)$$

where  $z$  is oriented in the direction of gravity. Here the transmissibilities are given by

$$D_{ev} = h_v D_{mv}, \quad D_{e\ell} = h_\ell D_{m\ell} \quad (11)$$

and

$$D_{m\ell} = \frac{k R_\ell \rho_\ell}{\mu_\ell}, \quad D_{mv} = \frac{k R_v \rho_v}{\mu_v} \quad (12)$$

The source and sink terms in equations (1) and (4) arise from bores, and if the total mass withdrawal,  $q_m$ , for each bore is specified, then the energy withdrawal,  $q_e$ , is determined as follows:

$$q_e = q_v h_v + q_\ell h_\ell \quad (13)$$

where

$$q_v = \sigma q_m, \quad q_\ell = (1 - \sigma) q_m \quad (14)$$

and

$$\sigma = \frac{1}{\left(1 + \frac{\rho_\ell R_\ell \mu_v}{\rho_v R_v \mu_\ell}\right)} \quad (15)$$

The form of equation (15) shows how important the relative permeability ratio  $R_\ell/R_v$  is in controlling the discharge composition. The relative permeability and capillary pressure functions are summarized in the next section, Constitutive Relationships.

In addition to the flow of heat and mass, FEHMN is also capable of simulating noncondensable gas flow (usually air) and passive tracer flow. The noncondensable gas conservation equation is

$$-\bar{\nabla} \cdot (C_\ell D_{m\ell} \bar{\nabla} p_\ell) - \bar{\nabla} \cdot (C_v D_{mv} \bar{\nabla} p_v) + \frac{\partial}{\partial z} g(C_\ell D_{m\ell} \rho_\ell + C_v D_{mv} \rho_v) + \frac{\partial A_c}{\partial t} + q_c = 0 \quad (16)$$

Here  $C$  is the concentration of the noncondensable gas and is expressed as a fraction of total mass. The term  $\bar{f}_c$  is the mass flux,  $q_c$  is the source (or sink) strength, and  $A_c$  is the accumulation term:

$$\bar{f}_c = C_v \rho_v \bar{V}_v + \rho_\ell \bar{V}_\ell C_\ell \quad (17)$$

$$q_c = C_v q_v + C_\ell q_\ell \quad (18)$$

$$A_c = \phi(S_v \rho_v C_v + S_\ell \rho_\ell C_\ell) \quad (19)$$

The passive tracer equation is not directly coupled to the pressure field but merely uses the pressure field obtained by the heat and mass transfer solution:

$$-\bar{\nabla} \cdot (C_\ell D_{m\ell} \bar{\nabla} p_\ell) - \bar{\nabla} \cdot (C_v D_{mv} \bar{\nabla} p_v) + \bar{\nabla} \cdot (D_c \bar{\nabla} C_\ell) + g \frac{\partial}{\partial z} (C_\ell D_{m\ell} \rho_\ell + C_v D_{mv} C_v) + \frac{\partial A_c}{\partial t} + q_c = 0 \quad (20)$$

(where the terms are defined analogously to the condensable gas equation terms) the additional term  $\bar{\nabla} \cdot (D_c \bar{\nabla} C_\ell)$  is the dispersion term. At present the code allows for up to 10 tracers.

**2. Constitutive Relationships.** In the equations described above the porosity, permeability, density, enthalpy, and viscosity can be strong functions of pressure and temperature. These functions make the code very nonlinear. In addition the relative permeabilities and capillary pressure can be strong functions of saturation.

The pressure and temperature dependent behavior of the density, enthalpy, and viscosity are represented by rational polynomials. Using a technique developed at the University of Auckland, New Zealand, accurate fits to the National Bureau of Standards (NBS) steam table data were obtained over the ranges:

$$0.001 \text{ MPa} \leq P \leq 110. \text{ MPa} \quad (21)$$

$$0.001^\circ \text{C} \leq T \leq 360^\circ \text{C}$$

The maximum error was 0.3% for all the functions. The rational polynomial representation proved to be both accurate and fast. For details the reader is referred to Zyvoloski and Dash (1991). In addition a low pressure thermodynamics set is provided with the ranges  $0.001MPa \leq P \leq 20MPa, 0.5^\circ C \leq T \leq 360^\circ C$ . The maximum error for this set is also 0.3%.

The tracer module of FEHMN has provisions for reactive tracers. At present four adsorption models have been included. These are the linear, Langmuir (Satter et al., 1980), Freundlich, and modified Freundlich isotherm models. The discussion follows the description given by Robinson (1988). With adsorption the equations describing the conservation of species, Eq. (16) is modified by the addition of the term

$$\rho_r \frac{\partial C_R}{\partial t}$$

where  $\rho_r$  is the rock density and  $C_R$  represents the adsorption of species onto the reservoir rock and is given by

$$C_R = \frac{\alpha_1 C_l^\beta}{1 + \alpha_2 C_l^\beta} \quad (22)$$

The terms in Eq. (22) are given in Table II where  $K_D$ ,  $A$ ,  $\beta$ ,  $C_{max}$ ,  $r_b$ , and  $r$  are parameters associated with the sorption models. The adsorption term is included in the tracer solution by replacing the  $A_c$  term, Eq. (19), with the new term

$$A_c = \phi(S_v \rho_v C_v + S_l \rho_l C_l) + \rho_r C_R \quad (23)$$

Chemical reactions are modeled by modifying the source term,  $q_c$  in Eq. (18), with the addition of the term  $q_{cR}$  given below:

$$q_{cR} = \frac{a_1 C_l^{a_2}}{a_3 + a_4 C_l} \quad (24)$$

---



---

**TABLE II. Sorption Isotherm Models**


---

Model	Expression	$\alpha_1$	$\alpha_2$	$\beta$
Linear	$C_R = K_D C_t$	$K_D$	0	1
Freundlich	$C_R = A C_t^\beta$	A	0	$0 < \beta < 1$
Modified Freundlich	$\frac{C_R}{C_{max} - C_R} = A C_t^\beta$	$C_{max}$	A	$0 < \beta < 1$
Langmuir	$C_R = \frac{r_b C_t}{1 + r C_t}$	$r_b$	r	1

---



---

where the quantities  $a_1$ ,  $a_2$ ,  $a_3$ , and  $a_4$  are user inputted parameters. The general case given in Eq. (24) can sometimes be replaced by a simpler expression  $q_{cR} = a_1(C_t - a_2)$ . Both of the models are addressed in the input section.

Several well known relative permeability functions are available to the user. They are the simple linear functions, the Corey (1954) relationships, and the Sandia functions (van Genuchten, 1980).

The linear functions are given by

$$\begin{aligned}
 R_\ell &= 0 & , S_\ell &\leq rp_1 \\
 R_\ell &= (S_\ell - rp_1)/(rp_3 - rp_1) & , rp_1 &< S_\ell < rp_3 \\
 R_\ell &= 1 & , S_\ell &\geq rp_3 \\
 R_v &= 0 & , S_v &\leq rp_2 \\
 R_v &= (S_v - rp_2)/(rp_4 - rp_2) & , rp_2 &< S_v < rp_4 \\
 R_v &= 1 & , S_v &\geq rp_4
 \end{aligned} \tag{25}$$

where  $rp_1$ ,  $rp_2$ ,  $rp_3$  and  $rp_4$  are user supplied quantities.

The Corey relative permeability functions are given by

$$\begin{aligned}
 R_\ell &= \hat{S}_\ell^4 \\
 R_v &= (1 - \hat{S}_\ell)^2(1 - \hat{S}_\ell^2)
 \end{aligned} \tag{26}$$

where  $\hat{S}_\ell = (S_\ell - rp_1 - rp_2)/(1 - rp_1 - rp_2)$  and where the input quantities  $rp_1$  and  $rp_2$  are the residual liquid and vapor saturations respectively.



The van Genuchten (van Genuchten, 1980) functions are described by the following formulae:

$$\begin{aligned}\hat{S} &= \frac{(S_t - rp_2)}{(rp_3 - rp_2)} \\ R_t &= \sqrt{\hat{S} [1.0 - (1.0 - (\hat{S})^{1/\lambda})^\lambda]^2}, \hat{S}_t < rp_3 \\ &= 1.0, \hat{S}_t \geq rp_3 \\ R_v &= 1.0 - R_t\end{aligned}\quad (27)$$

where  $\lambda = rp_1$  and  $rp_1, rp_2$  and  $rp_3$  are parameters supplied by the user.

Composite relative permeability curves, as described by Klavetter and Peters (1986), are also available. See Section III B, macro-command *RLP* for an input description.

$R_t$  and  $R_v$  are restricted by the relationships

$$0 \leq R_v \leq 1.0 \quad (28)$$

$$0 \leq R_t \leq 1.0$$

and the relative permeability functions are truncated to the appropriate value if the above conditions are violated.

The capillary functions included with FEHMN are the linear function and the Sandia capillary pressure model. Our terminology follows that of Pruess (1987).

The linear capillary function model is given by the following equations

$$\begin{aligned}P_{cap} &= cp_1, & S_t &\leq cp_2 \\ P_{cap} &= 0.0, & S_t &\geq cp_3 \\ P_{cap} &= cp_1 \frac{cp_3 - S_t}{cp_3 - cp_1}, & cp_2 &< S_t < cp_3\end{aligned}\quad (29)$$

where  $cp_1, cp_2$ , and  $cp_3$  are parameters supplied by the user. The restriction  $cp_3 > cp_2$  is also necessary.

The van Genuchten functions (van Genuchten, 1980) are described by the following equations

$$\begin{aligned}\hat{S} &= \frac{S_t - S_{tr}}{S_{ts} - S_{tr}} \\ P_{cap} &= 0, \quad S_t \geq cp_5 \\ P_{cap1} &= P_o \left\{ (\hat{S})^{-1/\lambda} - 1.0 \right\}^{1.0-\lambda} \\ P_{cap} &= P_{max}, \quad P_{cap1} \geq P_{max} \\ P_{cap} &= P_{cap1}, \quad P_{cap1} < P_{max}\end{aligned}\quad (30)$$

where  $\lambda = cp_1, P_o = 1.0/cp_3, P_{max} = cp_4, S_{ts} = cp_5, S_{tr} = cp_2$ .

The capillary pressure curves approach an infinite value as  $S_\ell$  approaches 0. This was observed by Nitao (1988) who suggested using Eq. (30) only to a value of one-half the maximum suction observed in the rock ( $P_{max}$ ) and linearly extrapolating the capillary pressure to the maximum capillary pressure at  $S_\ell = 0$ . We have also employed this technique in FEHMN.

The van Genuchten relative permeability curves and capillary pressure functions are the primary ones used for Yucca Mountain calculations.

If the flow of air is also modeled, appropriate thermodynamic information for air must also be provided. The density of air is assumed to obey the ideal gas law, using atmospheric conditions as our reference state we have

$$\rho_a = 1.292864 \left( \frac{273.0}{T + 273.0} \right) \left( \frac{P}{0.101325} \right) \quad (31)$$

where  $\rho_a$  has the units  $kg/m^3$ ,  $T$  is in  $^\circ C$ , and  $P$  is in  $MPa$ . The mixture density is given by

$$\rho_v = \rho_{v,w} + \rho_a \quad (32)$$

where  $\rho_{v,w}$  is the density of the water vapor. The density of the liquid phase is assumed to be unaffected by the amount of dissolved air it contains.

The enthalpy of air is a function of temperature only

$$\begin{aligned} C_{pa} &= 6122.0 - 11.76(T^*) + 0.0177(T^*)^2 \\ h_a &= C_{pa}(T \cdot 10^{-6}) \end{aligned} \quad (33)$$

where  $h_a$  is the enthalpy of air (MJ/kg),  $C_{pa}$  is the heat capacity of air (MJ/kg  $^\circ C$ ), and  $T^* = T + 273$ . The mixture enthalpy for the vapor phase is

$$h_v = h_{v,w}(1 - \eta_v) + h_a \eta_v \quad (34)$$

where  $h_{v,w}$  is the enthalpy of steam and  $\eta_v$  is the fraction by mass of air in the vapor phase. The enthalpy of the liquid phase is given by the enthalpy of the dissolved air, the heat of solution, and the enthalpy of the water. At present, we neglect the heat of solution and use the enthalpy of air described above:

$$h_\ell = h_{\ell,w}(1 - \eta_\ell) + h_a \eta_\ell \quad (35)$$

where  $h_{\ell,w}$  is the enthalpy of liquid water and  $\eta_{\ell}$  is the mass fraction of  $a$  in the liquid phase.

Assuming ideal gas behavior, the mass fraction of air in the vapor phase may be expressed as

$$\eta_v = \frac{\rho_a}{\rho_v}$$

the mass fraction of air in the liquid phase is assumed to obey Henry's law or

$$\eta_e = \alpha P_a$$

where  $\alpha$  is the Henry's law constant ( $\alpha = 1.611 \times 10^{-4} P_a^{-1}$ ) for air and  $P_a$  is the partial pressure of air.

The viscosity of the vapor phase is assumed to be a linear combination of the air viscosity and the water viscosity

$$\mu_v = \mu_{v,w}(1 - \eta_v) + \mu_a \eta_v \quad (36)$$

where  $\mu_{v,w}$  is the steam viscosity and is obtained from steam data. The viscosity of air is assumed constant

$$\mu_a = 1.82 \times 10^{-5} \text{ cp} \quad (37)$$

The liquid phase viscosity is assumed to be independent of the amount of dissolved air and is obtained from steam table data:

$$\mu_{\ell} = \mu_{\ell,w} \quad (38)$$

Often it is necessary to accommodate changes in the rock porosity and permeability due to changes in effective stress caused by temperature and pore fluid pressure changes. A linear and nonlinear model are currently incorporated into the code for this purpose.

The linear pore pressure model for porosity is given by

$$\phi = \phi_o + (1 - \phi_o)(c_r - c_g)(P - P_o) \quad (39)$$

where  $\phi$  is the porosity at pressure  $P$ ,  $\phi_o$  is the initial porosity at pressure  $P_o$ ,  $c_r$  is the pore volume compressibility of the rock and  $c_g$  is the compressibility of the matrix grain material.

The nonlinear model for porosity (Gangi, 1978) currently used in the code is given by

$$\phi = \phi_o \left[ 1 - \left( \frac{P_c}{P_o} \right)^m \right] \quad (40)$$

and

$$P_c = \sigma - P - \alpha E \Delta T \quad (41)$$

where  $P_c$  is the closure stress,  $\sigma$  is the *in situ* stress (assumed isotropic),  $\alpha$  is the coefficient of thermal expansion of the rock,  $E$  is Young's modulus,  $\Delta T$  is the temperature change and  $P_o$  and  $m$  are parameters in the model.

For either case the effect of stress and temperature changes on permeability are modeled with

$$k = k_o \left( \frac{\phi}{\phi_o} \right)^3 \quad (42)$$

where  $k$  is the permeability at porosity  $\phi$ .

### C. Discretization of the Governing Equations

The time derivatives in the Eqs. (1-42) are discretized using the standard first order method given by

$$f(t^{n+1}) = f(t^n) + \Delta t \left( a f'(t^{n+1}) + (1 - a) f'(t^n) \right) \quad (43)$$

where  $f(t^{n+1})$  is the desired function at time  $t^{n+1}$ ,  $f(t^n)$  is the known value of  $f$  at time  $t^n$ ,  $\Delta t$  is the time step,  $f'$  is the derivative of  $f$  with respect to time and  $a$  is a weighting factor. For  $a = 1$ , the scheme is fully implicit (backward Euler) and for  $a = 0$ , the scheme is fully explicit (forward Euler).

The space derivatives in the governing equations are discretized using the finite element formulation. The finite element equations are generated using the Galerkin formulations. For a detailed presentation of the finite element method the reader is referred to Zienkiewicz (1977). In this method the flow domain,  $\Omega$ , is assumed to be divided into finite elements; and variables  $P$ ,  $h$  and  $T$ , along with the accumulation terms  $A_m$  and  $A_e$ , are interpolated in each element:

$$P = [N]\{P\}, \quad h = [N]\{h\}, \quad T = [N]\{T\}, \quad A_m = [N]\{A_m\}, \quad \text{and} \quad A_e = [N]\{A_e\}$$

where  $[N]$  is the shape function. Here  $h$  is used to represent the generalized energy variable;  $T$  in single phase water states,  $S$  in 2-phase water states.

These approximations are introduced in Eqs. (9), (10), and (20), and the Galerkin formulation (described by Zienkiewicz and Parekh, 1970) is applied. The following equations are derived:

$$[T_m(P, h)]\{P\} + \hat{C} \frac{\partial A_m}{\partial t} + \{q_m\} - g\{R_m\} = \{F_m\} \quad (44)$$

and

$$[T_e(P, h)]\{P\} + [K]\{T\} + \hat{C} \frac{\partial A_e}{\partial t} + \{q_e\} - g\{R_e\} = \{F_e\} \quad (45)$$

where

$$T_{mij} = \int_{\Omega} \bar{\nabla} N_i \cdot D_m^{UP} \bar{\nabla} N_j dV \quad , \quad (46)$$

$$T_{eij} = \int_{\Omega} \bar{\nabla} N_i \cdot D_e^{UP} \bar{\nabla} N_j dV \quad , \quad (47)$$

$$K_{ij} = \int_{\Omega} \bar{\nabla} N_i \cdot \bar{\nabla} N_j dV \quad , \quad (48)$$

$$\hat{C}_{ij} = \int_{\Omega_j} N_i N_j dV \quad , \quad (49)$$

$$R_{mi} = \int_{\Omega_j} \frac{\partial N_i}{\partial y} N_j D_m^{UP} \rho_m dV \quad , \quad (50)$$

and

$$R_{ei} = \int_{\Omega_j} \frac{\partial N_i}{\partial y} N_j D_e^{UP} \rho_e dV \quad . \quad (51)$$

Equations (50) and (51) need some comment. The term  $D_e^{UP}$  indicates an upstream-weighted transmissibility (Dalen, 1979). This technique has worked well in the low-order elements (3-node triangle, 4-node quadrilateral), where the schemes resemble difference techniques. The upstream weighting is determined by comparing the velocities at the nodes  $i$  and  $j$ . The shape function coefficients are generated in a unique way that requires the integrations in Eqs. (50) and (51) to be performed only once and the nonlinear coefficients to be separated from this integration. The reader is referred to Zyvoloski (1983) for more details.

The integration scheme used in this report is similar to that described by Young (1981). His implementation differs from common methods in that it uses Lobatto instead of Gauss integration. The net effect is that, while retaining the same order of integration accuracy (at least for linear and quadratic elements), there are considerably fewer nonzero terms in the resulting matrix equations. Figure 1 shows a comparison of the nodal connections for Lobatto and Gauss integration methods. It should be noted that these results hold on an orthogonal grid only. If a nonorthogonal grid were introduced, then additional

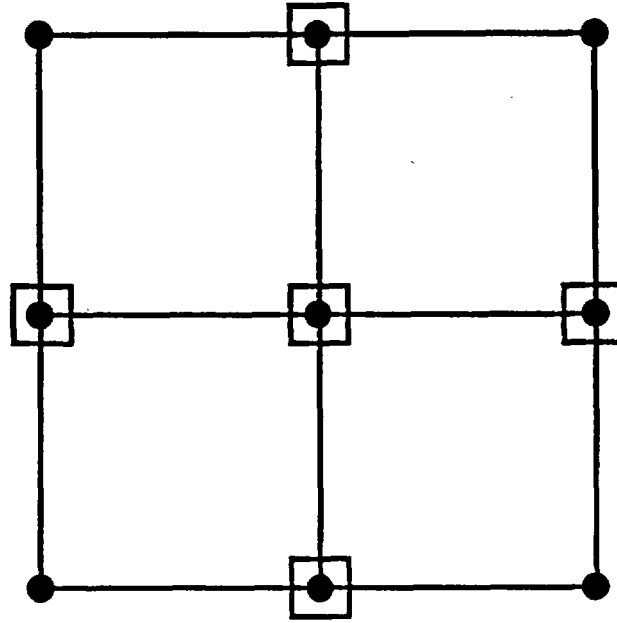


Fig. 1. Comparison of nodal connections for conventional and Lobatto integrations for an orthogonal grid.

nonzero terms would appear in the Lobatto quadrature method. Note also that the linear elements yield the standard 5- or 7-point difference scheme. The reader is referred to Young's paper for more details.

A similar approach is used to solve the transport equation. Following the discussion above the species concentration,  $C$ , and the species accumulation term,  $A_c$ , are interpolated in each element.

$$C = [N]^T \{C\}, \quad A_c = [N]^T \{A_c\}$$

Using these approximators and using a Galerkin approach, we obtain the following equation

$$[T_c(C)]\{P\} + [D_c]\{C\} + \hat{C} \frac{\partial A_c}{\partial t} + \{q_c\} + \{R_c\} = \{F_c\} \quad (52)$$

when

$$T_{cij} = \int_{\Omega} \bar{\nabla} N_i \cdot D_m C_{ij}^{UP} \bar{\nabla} N_j dv \quad (53)$$

$$D_{cij} = \int_{\Omega} \bar{\nabla} N_i \cdot D_c \bar{\nabla} N_j dv \quad (54)$$

$$R_{cij} = \int_{\Omega} \frac{\partial N_i}{\partial y} \cdot D_m C_{ij}^{UP} \bar{\nabla} N_j dv \quad (55)$$

where  $C_{ij}$  was defined previously and  $C_{ij}^{UP}$  is an upstream weighted species concentration. This approach is similar to the finite difference method for solving the transport equations.

#### D. Boundary Conditions

Two mass flow boundary conditions are allowed in FEHMN. They are no flow and specified variable values. The no flow conditions are automatically satisfied by the finite element mesh. Specified variable quantities are obtained in the following manner. A pressure dependent flow term is used:

$$q_i = I_i(P_{flow,i} - P_i) \quad (56)$$

where  $P_i$  is the pressure at node  $i$ ,  $q_i$  is the flow rate,  $I_i$  is the impedance, and  $P_{flow,i}$  is the specified flowing pressure at node  $i$ . By specifying a large  $I_i$ , we can force the pressure to be equal to  $P_{flow,i}$ . The energy (or temperature) specified at node  $i$  refers only to the incoming fluid value, if fluid flows out of the reservoir, stability dictates that the energy of the in-place fluid be used in the calculations. Species concentration is handled in a manner analogous to the energy variable. Only the incoming species concentration can be specified; if the flow is out of the reservoir the in-place species concentration is used.

In addition to the mass flow boundary conditions, heat flow boundary conditions are also provided. A specified heat flow can be input or a specified temperature obtained

$$q_{e,i} = I_{e,i}(T_{flow,i} - T_i)$$

where  $T_i$  is the nodal temperature,  $T_{flow,i}$  is the specified flowing temperature at node  $i$ ,  $I_{e,i}$  is the impedance to heat flow at node  $i$ , and  $q_{e,i}$  is the heat flow at node  $i$ . This heat flow is superimposed on any existing heat flow from the other boundary conditions or source terms.

#### E. Solution Methods

The application of the discretization methods to the governing partial differential equations yields a system of nonlinear algebraic equations. To solve these equations, the Newton-Raphson iterative procedure is used. This is an iterative procedure that makes use of the derivative information to obtain an updated solution from an initial guess. Let the set equations to be solved be given by

$$\overline{F}(\overline{x}) = 0 \quad (57)$$

where  $\overline{x}$  is the vector of unknown values of the variables that satisfy the above equation. The procedure is started by making an initial guess at the solution, say  $\overline{x}^0$ . This is usually taken as the solution from the previous time step. Denoting the value of  $\overline{x}$  at the  $k$ th iteration by  $\overline{x}^k$ , the updating procedure is given by

$$\overline{x}^{(k+1)} = \overline{x}^k - \overline{F}(\overline{x}^k) \left( \frac{\partial \overline{F}}{\partial \overline{x}^k} \right)^{-1} . \quad (58)$$

At each step, the residuals  $\overline{F}(\overline{x}^k)$  are compared with a prescribed error tolerance. The prescribed error tolerance,  $\epsilon$ , is an input parameter and an  $\ell^2$  norm is used:

$$\|F\|_k = \left( \sum_i F_i^2 \right)_k^{1/2} .$$

Convergence is achieved when

$$\|F\|_k \leq \epsilon \|F\|_0 .$$

$\epsilon$  is usually in the range  $10^{-4}$ - $10^{-7}$ . Semiautomatic timestep control is designed based on the convergence of the Newton iterations. If the code is unable to find a solution  $\overline{x}^k$  such that the residuals become less than the tolerance within a given number of iterations, the time step is reduced and the procedure repeated. On the other hand, if convergence is rapid, the timestep is increased by multiplying with a user supplied factor, thus allowing for large timesteps when possible.

The matrix equation to be solved at each Newton-Raphson iteration has the form

$$[A]\{x\} = \{b\} , \quad (59)$$

where  $[A]$  is the Jacobian matrix,  $\{x\}$  is the solution vector, and  $\{b\}$  is the residual. The  $[A]$  matrix is sparse and banded. For computation,  $\{x\}$  is replaced by  $\{\delta x\} = \{x\}^{n+1} - \{x\}^n$ , and  $\{b\}$  is replaced by  $\{r\} = \{b\} - [A]\{x\}^n$ , where  $n$  is the iteration number. (Note that this is different from the overall Newton iteration.) Thus, only changes in  $\{x\}$  are calculated.

Complete Gaussian elimination or factorization on Eq. (59) would result in fill-in of all the bands between the lowest subdiagonal and the highest superdiagonal bands. Incomplete factorization involves finding only approximate upper and lower triangular matrices  $\tilde{L}$  and  $\tilde{U}$ , requiring very little fill-in. The computing effort for obtaining the incomplete factors is much less than for the complete factors. However, an iterative procedure is now



required. The presentation of the theory below follows that of Saad and Schultz (1986). The matrix  $[A]$  is partially factored into upper and lower triangular form

$$[\bar{A}] = [\tilde{L}][\tilde{U}] , \quad (60)$$

where  $[\bar{A}] \neq [A]$  because, in general,  $[\tilde{L}]$  and  $[\tilde{U}]$  will contain only some of the steps of the elimination process. To incompletely factor a matrix, a prior knowledge of the fill-in pattern is required. A symbolic factorization is performed (just once) to establish where the fill-in occurs and to determine the order of each term. Figure 2 shows a matrix and its first level of fill (0's) resulting from factorization of the original matrix elements (x's). We could continue the process to get higher-order terms, but usually the lower-order terms are all that are necessary (Zyvoloski, 1986). The amount of factorization is limited by computer storage considerations. Once factored, the solution is easy to carry out as it consists of a forward and a backward substitution:

$$\{v\} = [\tilde{U}]^{-1} \left\{ [\tilde{L}]^{-1} \{r\} \right\} \quad (61)$$

where  $\{v\}$  is the approximate change in  $\{x\}$ . The following recursion scheme is used to refine the approximation:

$$\{v\}^{n+1} = [\bar{A}]^{-1} \{r\}^n = [\tilde{U}]^{-1} \left\{ [\tilde{L}]^{-1} \{r\}^n \right\} , \quad (62)$$

$$\{x\}^{n+1} = \{x\}^n + \{v\}^{n+1} , \quad (63)$$

$$\{r\}^{n+1} = \{r\}^n - [\bar{A}]\{v\}^{n+1} \quad (64)$$

where  $n$  is the iteration index and  $\{x\}^0 = 0$  since the original matrix equation is written in residual form [see paragraph after Eq. (59)]. The solution scheme, comprising Eqs. (61)-(64), may be accelerated by over-relaxation procedures, but it is better to use orthogonalization-minimization. If the Jacobian matrix were symmetric, conjugate gradient could be used. For nonsymmetric matrices, the GMRES (Generalized Minimal Residual Equation Solver) procedure (Saad and Schultz, 1986) is used.

For comparison purposes, the simple over-relaxation procedure is discussed first. In the recursion scheme [Eqs. (62)-(64)], Eq. (63) is replaced by  $\{x\}^{n+1} = \{x\}^n + w\{v\}^{n+1}$ , and Eq. (64) is replaced by  $\{r\}^{n+1} = \{r\}^n - w[A]\{v\}^{n+1}$ . Here  $w$  is the over-relaxation parameter and satisfies the relation  $1 < w < 2$ . After Eq. (64) is calculated, the procedure returns to Eq. (61) and continues until  $\{r\}^{n+1}$  is reduced to some predetermined value. For many reservoir problems, convergence is extremely slow, and the ortho-minimization procedures provide a valuable alternative.

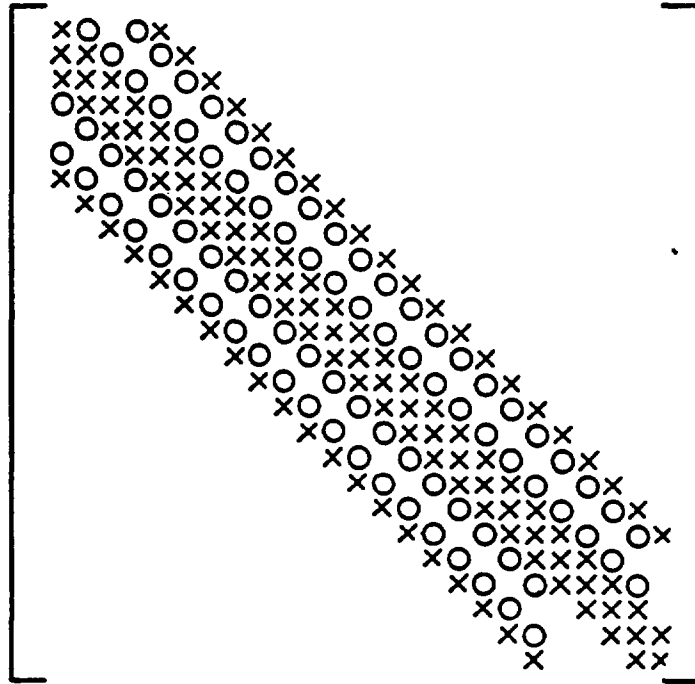


Fig. 2. Matrix band structures showing second-order fill-in.  
 x - original matrix positions.  
 o - fill-in with order 2 factorization.

The GMRES algorithm is

1. Set  $\{r\}^\circ = \{b\}$  and set  $\{v\}^1 = \{r\}^\circ / \|\{r\}^\circ\|$  where  $\|\{r\}\|$  is the sum squared norm ( $\|\{r\}\| = \{\sum_{i=1}^n r_i\}^{1/2}$ ) of  $\{r\}$  and  $n$  is the number of unknowns. We also assume that  $\{x\}^\circ = \{0\}$ .
2. Perform orthogonalization calculation,  $m = 1, \text{NORTH}$

$$\{w\}^{m+1} = [A]\{v\}^m - \sum_{i=1}^m ([A]\{v\}^i, \{v\}^i) \{v\}^i \quad (65)$$

$$h_m^{m+1} = \|\{w\}^{m+1}\| \quad (66)$$

$$\{v\}^{m+1} = \{w\}^{m+1} / h_m^{m+1} \quad (67)$$

Where NORTH is the maximum number of orthogonalizations allowed.

3. Form approximate solution ( $n = \text{NORTH}$ )

$$\{x\}^m = \{x\}^\circ + [V]^m \{y\}^m \quad (68)$$

where  $[V]^m$  is an  $n$  by  $m$  matrix which contains the  $\{v\}^i$  ( $i = 1, m$ ) and  $\{y\}^m$  is an  $n$  dimensional vector which minimizes the function.

$$f(y) = \|B\{e\}^1 - [H]^m\{y\}\| \quad (69)$$

Here  $B = \|r^\circ\|$ ,  $\{e\}^1$  is the unit vector, and  $[H]^m$  is a  $k + 1$  ( $= n$ ) by  $k$  matrix whose only nonzero entries are the  $h_i^{i+1}$  calculated in Eq. (66). This minimization is economically done using  $Q - R$  factorization. (See Saad and Shultz, 1986, for details.)

4. Calculate  $\|\hat{r}_m\|$  where

$$\{r\}^m = \{b\} - [A]\{x\}^m \quad (70)$$

If  $\|r_m\| \leq \epsilon$ , some specified tolerance, then the process is complete. Otherwise we set  $\{x\}^\circ = \{x\}^m$ ,  $\{v\}^1 = \{r\}^m / \|\{r\}^m\|$  and proceed from Eq. (65) of the GMRES algorithm. There is an intimate relationship between the outer iteration (Newton-Raphson) and the inner iteration (solution of linear equations). If the outer iteration is far from convergence, we can solve the linear system of equations with a rather large tolerance. As the outer iterations converge we must likewise have a finer tolerance for the inner iteration. The method used here is one developed by Diaz, Jines, and Steihaug (1985). Regions of linear and quadratic convergence are defined, and multipliers for the square of the residuals and the residuals are specified. Comparing the magnitude of the terms determines the largest possible tolerance for the inner iteration.

A mathematical theory similar to that for conjugate gradient methods (for example, showing a reduction in condition number with each iteration) is not available. In basic terms the  $h_m^{m+1}$  in Eqs. (66) and (67) ensure that the  $\{v\}^i$  are orthogonal and that the  $\{y\}^m$  in Eqs. (68) and (69) are such that the square of the  $\{r\}^{n+1}$  is minimized. For more details the reader is referred to Meijerink and Van der Vorst (1981), Behie and Forsythe (1984), and Behie and Vinsome (1982). To minimize the storage required, the procedure is restarted after every NORTH iteration. The more orthogonalizations before restarting, the faster the convergence, but this benefit must be weighed against the greater storage and longer running time required for the additional orthogonalizations.

## F. Dual Porosity Formulation

Many problems are dominated by fracture flow. In these cases the fracture permeability controls the pressure communication in the reservoir even though local storage around the fracture may be dominated by the porous rock which communicates only with the closest fractures. Moench (1984) has studied several wells in the saturated zone beneath Yucca Mountain and found the results could be understood if dual porosity methods were used. Figure 3 depicts the dual porosity concept. The computational volume in the figure

consists of a fracture which communicates with fractures in other computational cells, and matrix material which only communicates with the fracture in its computational cells. This behavior of the matrix material is both a physical limitation and a computational tool. The physical limitation results from the model's inability to allow the matrix materials in different cells to communicate directly. This yields only minor errors in saturated zone calculations, but could pose larger errors in the unsaturated zone where capillary pressures would force significant flow to occur in the matrix material. The computational advantages will be addressed at the end of this section.

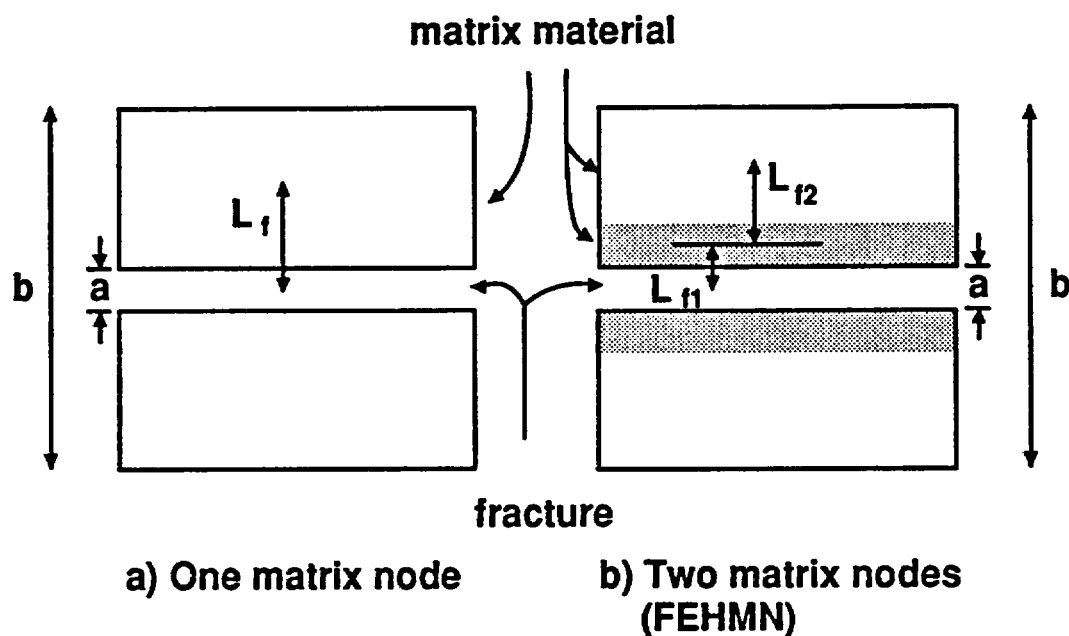


Fig. 3. Computational volume element showing dual porosity parameters.

Two parameters characterize a dual porosity reservoir. The first is the volume fraction,  $V_f$ , of the fractures in the computational cell. For the simple system shown in Fig. 3a this fraction is  $a/b$ . The second parameter is related to the fracture's ability to communicate with the local matrix material. In the literature this parameter takes a variety of forms. The simplest is a length scale,  $L_f$ . This quantifies the average distance the matrix material is from the fracture. This length scale is also shown in Fig. 3a. With just one node in the matrix material the transient behavior in the matrix material cannot be modeled. To improve this situation, two nodes are used in FEHMN to represent the matrix material. Conceptually, this is the same formulation as just described with only additional fracture volume needed (it is assumed the length scale of each matrix volume is proportional to the volume fraction). This is shown in Fig. 3b. More matrix nodes could be added, but data is rarely good enough to justify the use of even two matrix nodes. We note here that the

simple slab model depicted in Fig. 3 is just one of several different geometric arrangements. Moench (1984) and Warren and Root (1963) list other reservoir types. All of them are similar in the assumption of a local one dimension connection of the matrix to the fracture.

Computationally, the volume fraction and length scale are used to create one dimensional versions of Eq. (9), Eq. (10), Eq. (16), and Eq. (20). The length scale is used to modify spacial difference terms and the volume factors are used to modify the accumulation terms [the  $\hat{C}$  matrix in Eq. (44)]. The volume fractions for FEHMN are given by

$V_f = 1 - V_{f1} - V_{f2}$ , volume fraction of fractures

$V_{f1}$  - fraction of first matrix volume (input)

$V_{f2}$  - fraction of second matrix volume (input)

the length scales are given by

$L_f = L_{f0}V_f$ , length scale for the fracture volume

$L_{f0}$  - length scale (input)

$L_{f1} = L_{f0}V_{f1}$  length scale of first matrix volume

$L_{f2} = L_{f0}V_{f2}$ , length scale of second matrix volume

The geometric factor representing the spacial differencing of the one dimensional equation for flow between the fracture and the first matrix node [analogous to the geometric part of Eq. (46) and Eq. (47)] is given by

$$T_{ff1} = \frac{1.0}{L_{f1}}(L_{f1} + L_f) \quad (71)$$

The analogous term for the flow from the first matrix volume to the second matrix volume is given by

$$T_{f1f2} = \frac{1.0}{L_{f2}}(L_{f1} + L_{f2}) \quad (72)$$

The one dimensional nature of the equations provides a computationally efficient method to solve the algebraic equations arising from the dual porosity simulation. Equation (73) shows the matrix equation arising from a dual porosity simulation.

$$\begin{bmatrix} A_{00} & A_{01} & A_{02} \\ A_{10} & A_{11} & A_{12} \\ A_{20} & A_{21} & A_{22} \end{bmatrix} \begin{Bmatrix} P_0 \\ P_1 \\ P_2 \end{Bmatrix} = - \begin{Bmatrix} R_0 \\ R_1 \\ R_2 \end{Bmatrix} \quad (73)$$

Here the subscript 0 refers to the fracture, 1 refers to the first matrix volume, and 2 refers to the second matrix volume.

The  $P$  represents the unknown variable or variable pair. The one dimensional character of the matrix diffusion means that the second matrix node can only depend on the first

matrix node. Therefore, the submatrix  $A_{20}$  is empty. The fact that matrix nodes cannot communicate with matrix nodes in other computational cells means that the submatrices  $A_{21}$  and  $A_{22}$  are diagonal. Therefore we may write

$$\{P_2\} = [A_{22}]^{-1}[-\{R_2\} - [A_{21}]\{P_1\}] \quad (74)$$

where the inversion is trivial because  $[A_{22}]$  is diagonal. Substituting this expression into the equation for the first matrix node we have

$$[A_{10}]\{P_0\} + [A_{11}]\{P_1\} + [A_{12}][A_{22}]^{-1}\{-\{R_2\} - [A_{21}]\{P_1\}\} = -\{R_1\} \quad (75)$$

Rearranging, we have

$$[A_{10}]\{P_0\} + \left[ [A_{11}] - [A_{12}][A_{22}]^{-1}[A_{21}] \right] \{P_1\} = -\{R_1\} + [A_{12}][A_{22}]^{-1}\{R_2\}$$

or

$$\{P_1\} = [\tilde{A}_{11}]^{-1}[\{\tilde{R}_1\} - [A_{10}]\{P_0\}] \quad (76)$$

where

$$[\tilde{A}_{11}] = [A_{11}] - [A_{12}][A_{22}]^{-1}[A_{21}]$$

and

$$\{\tilde{R}_1\} = -\{R_1\} + [A_{12}][A_{22}]^{-1}\{R_2\}$$

where the inversion and multiplications are trivial because of the diagonal nature of the matrices involved. Equation (76) may next be substituted into the equation for the fracture variables. Noting that  $[A_{02}]$  is empty (the fracture can only communicate with the first matrix volume) we have

$$[A_{00}]\{P_0\} + [A_{01}][\tilde{A}_{11}]^{-1}\left\{ \{\tilde{R}_1\} - [A_{10}]\{P_0\} \right\} = -\{R_0\} \quad (77)$$

Rearranging terms we have

$$\left[ [A_{00}] - [A_{01}][\tilde{A}_{11}]^{-1}[A_{10}] \right] \{P_0\} = -\{R_0\} + [A_{01}][\tilde{A}_{11}]^{-1}\{\tilde{R}_1\} \quad (78)$$

Equation (78) consists of an augmented fracture matrix of the same form as the original fracture matrix  $[A_{00}]$ . The operations carried out only add a few percent to the solution time required to solve a single porosity system. After the solution of Eq. (78) is obtained with the methods described in Section E, the solution in the fracture volume can be obtained by using Eq. (74) and Eq. (76).

## II. CODE DESCRIPTION

In this section we present three important descriptions of FEHMN. First descriptions of all the subroutines are presented. Next the common block variables and calling parameters are described. Finally, the subroutine call tree structure for FEHMN is provided.

### A. Subroutines

The main program of the code FEHM is GZ. This program calls subroutine DATA to initialize most of the common block variables and calls subroutine INPUT which initializes most non-array variables and directs the data input. GZ also performs one time startup calculations: scaling of some variables, directing the calculation of element coefficient arrays, and the setting up of equation solution schemes. The major time step loop is contained within GZ. In this loop the model equations are solved at each time step, solution parameters adjusted, and variables updated for the next time step. Plotting data is also output from this loop.

The following subroutines are called from GZ (excluding calls to intrinsic functions): ANONP, BNSWER, COEFFC, CONCEN, CONTR, CO2CTR, DATA, DATCHK, DISK, DUAL, ENTHP, INPUT, NEAR3, PEINT, PLOT, RADIUS, RARNG, RESETV, SETORD, SICE, SLVESU, STEADY, STORSX, STRESS, TIMCRL, TYMING, USER, VARCHK, VELOC, WELBOR, WRTOU.

Table III contains a complete alphabetical listing of the FEHMN subroutines. A brief description of each routine is provided along with listings of which subroutines call the given routine and which subroutines it calls (intrinsic functions are excluded).

---



---

TABLE III. Subroutine Calls Within FEHMN

---

Name	Description	Calls	Called by
ANONP	Categorize elements. Call routines to generate finite element coefficients.	GENCOF	GZ
BNSWER	Call routines to assemble finite element equations and solve for the Newton-Raphson equations.	VARCHK, OUTBND, GENSL13, GENSL14, GENSL1	INPUT, THRMWC, THERMW
CAPPR	Calculate capillary pressure functions.		GZ, THRMWC
CNSWER	Call routine to generate tracer transport equations. Call tracer equation of state routines.	THERMC, GENCON	CSOLVE

---



---

**TABLE III. Subroutine Calls Within FEHMN**


---

<b>Name</b>	<b>Description</b>	<b>Calls</b>	<b>Called by</b>
<b>COEFFC</b>	Change coefficients of polynomial fits of the thermodynamic properties specified.		<b>GZ</b>
<b>CONCEN</b>	Organize calls required to run tracer transport model.	<b>RDCON, CSOLVE, WRTCN, PLOTG, DISKC, CONTRC</b>	<b>GZ, WRTOU, DISK, INPUT, CONTR, GENCON</b>
<b>CONEQ1</b>	Generate the equations of tracer transport.		
<b>CONTR</b>	Write out data for time history plots at particular nodes.	<b>CONCEN, VELOC</b>	<b>GZ, TIMCRL</b>
<b>CONTRC</b>	Write out tracer data for contour plots.		<b>CONCEN</b>
<b>CO2CTR</b>	Read input for noncondensable gas and initialize variables associated with the noncondensable gas.	<b>PSAT</b>	<b>GZ, TIMCRL, WRTOU, INPUT</b>
<b>CSOLVE</b>	Organize tracer solution so smaller time steps can be used for the tracer solution than for the flow solution.	<b>CNSWER, PLOTG1, THERMC</b>	<b>CONCEN</b>
<b>DATA</b>	Initialize common block variables.		<b>GZ</b>
<b>DATCHK</b>	Initial value analysis and data check.		<b>GZ</b>
<b>DISK</b>	Read and/or write to files for restart purposes.	<b>CONCEN, STRESS</b>	<b>GZ, TIMCRL</b>
<b>DISKC</b>	Read and write restart files for tracer variables.		<b>CONCEN</b>
<b>DUAL</b>	Read dual porosity data. Initialize dual porosity variables.	<b>VARCHK, DUALFA, DUALEX</b>	<b>GZ, TIMCRL, GENSL4, GENSL1, INPUT</b>
<b>DUALEX</b>	Extract dual porosity solution from primary variable solution.		<b>DUAL</b>



---



---

**TABLE III. Subroutine Calls Within FEHMN**


---

<b>DUALFA</b>	Assemble and load dual porosity solution and modify primary variables solution to account for dual porosity effects.	<b>VARCHK, GENEQ1, GENEQ3</b>	<b>DUAL</b>
<b>ENTHP</b>	Calculate the temperature for a given input enthalpy.		<b>GZ, STEADY</b>
<b>GENCOF</b>	Call routines to generate finite element coefficients. Perform the numerical integration of the elements.	<b>GNCF3, GNCF2</b>	<b>ANONP</b>
<b>GENCON</b>	Call routines to generate tracer equations. Call solver to obtain Newton-Raphson equations for tracer variables.	<b>CONEQ1, SOLVE, RD1DOF</b>	<b>CNSWER</b>
<b>GENDAT</b>	Generate coordinates and element information in simple geometric problems.		<b>INPUT, ZONE</b>
<b>GENEQC</b>	Generate equations for Newton-Raphson corrections for the water and non-condensable gas flow.		<b>GENSL4</b>
<b>GENEQ1</b>	Generate equations for Newton-Raphson corrections for water/vapor flow with no noncondensable gas.		<b>DUALFA, GENSL1</b>
<b>GENEQ3</b>	Generate equations for Newton-Raphson corrections for heat conduction only (i.e., permeability).		<b>DUALFA, GERSL4, GENSL1, GENSL3</b>
<b>GENSL1</b>	Call routines to generate the Newton-Raphson equations for water only problems. Call equation solver subroutine.	<b>GENEQ1, GENEQ3, DUAL, NORMAL, SOLVE2, RD2DOF</b>	<b>BNSWER</b>
<b>GENSL3</b>	Call routines to generate the Newton-Raphson equations for heat conduction only. Call equation solver routine.	<b>GENEQ3, SOLVE, RD1DOF</b>	<b>BNSWER</b>
<b>GENSL4</b>	Calls routines to generate equations for water/noncondensable gas problems and calls equation solver.	<b>GENEQC, GENEQ3, DUAL, NORMAL, SOLVE3, RD3DOF</b>	<b>BNSWER</b>

**TABLE III. Subroutine Calls Within FEHMN**

<b>Name</b>	<b>Description</b>	<b>Calls</b>	<b>Called by</b>
<b>GEOIN</b>	Reads element and coordinate information from MARC preprocessor.	INPUT,ZONE	
<b>GNCF2</b>	Generate 2-D finite element coefficients.	SHAP2R	GENCOF
<b>GNCF3</b>	Generate 3-D finite element coefficients.	SHAP3R, SHAP3P	GENCOF
<b>INPUT</b>	Initialize variables, read input, write out some input information.		CAPPR,CONC CO2CTR,DUA GENDAT,GEC IOFILE,PORO RLPERM, SIC STHER,STRES USER,WELBO ZONE
<b>IOFILE</b>	Open up initial pressure distribution when gravity is present (enabled).		INPUT
<b>LUDBKSB</b>	Performs forward and rock substitution for $N$ degree of freedom matrix elements.	SOLVEN	
<b>LUDCOMP</b>	Performs Gauss elimination on $N$ degree of freedom matrix elements.	SOLVEN	
<b>NEAR3</b>	Finds nearest node to a set of coordinates.	GZ	
<b>NELMFL</b>	Load nodal connection array.		GENCOF
<b>NOPCNR</b>	Identify form of incomplete LU decomposition matrix for the Newton-Raphson solution matrix with re-ordering of the node numbering.		SLVESU
<b>NOPCNV</b>	Identify form of LU decomposition matrix for the Newton-Raphson solution matrix with no recording of the node numbers.		SLVESU
<b>NORMAL</b>	Normalize Newton-Raphson equations and calculates sum-squared sum of residuals.		GNSL4, GENS

---



---

**TABLE III. Subroutine Calls Within FEHMN**


---

<b>Name</b>	<b>Description</b>	<b>Calls</b>	<b>Called by</b>
<b>OUTBND</b>	Test the dependent variables to determine if they are within the bounds set by the thermodynamics properties.		<b>BNSWER</b>
<b>PEINT</b>	Set up initial temperature gradients where gradient information is user specified.		<b>GZ</b>
<b>PLOT</b>	Write out data for time history plots at particular nodes.		<b>GZ, TIMCRL</b>
<b>PLOTCl</b>	Write out tracer data for time history plots. Print out at flow time steps.		<b>CONCEN RDCON</b>
<b>POROSI</b>	Read in data for pressure dependent porosity and permeability models. Calculate porosity and permeability functions.	<b>ROCK</b>	<b>INPUT, WRTOUT, THERMW</b>
<b>PSAT</b>	Calculate the saturation pressure of water for a given temperature.		<b>VARCHK, CO2CTR, THRMWC GZ</b>
<b>RADIUS</b>	Modify finite element coefficients to obtain a radial model.		<b>GZ</b>
<b>RARNG</b>	Rearrange 3-D coordinates to obtain 2-D problems when enabled.		<b>GZ</b>
<b>RDCON</b>	Read in tracer data. Initialize tracer variables.	<b>THERMC PLOTCl</b>	<b>CONCEN</b>
<b>RD1DOF</b>	Solves the equations generated for heat conduction by a reduced degree of freedom method.	<b>SOLVE</b>	<b>GENSL3, GENCON</b>
<b>RD2DOF</b>	Solve the equations generated for the water only problems by the reduced degree of freedom method.	<b>SOLVE</b>	<b>GENSL1</b>
<b>RD3DOF</b>	Solve the equations generated for water/noncondensable gas problems by the reduced degree of freedom method.	<b>SOLVE2, SOLVE</b>	<b>GENSL4</b>

TABLE III. Subroutine Calls Within FEHMN

Name	Description	Calls	Called by
RESETV	Reset the dependent variables to the last time step value. Used when iteration limits are exceeded and a particular time step is restarted.		GZ
RLPERM	Calculate relative permeability functions.		GZ, THRMWC, THERMW
SFN2R	Interpolation routine used by ZONE (2-D).		ZONE
SFN3R	Interpolation routine used by ZONE (3-D).		ZONE
SHAP2R	Evaluate 2-D finite element shape functions at quadrature points.		GNCF2
SHAP3P	Evaluate 3-D prism elements at quadrature points.		GNCF3
SHAP3R	Evaluate 3-D finite elements shape functions at quadrature points.		GNCF3
SICE	Reads in data for simulation with ice present.	STHER	GZ,WRTOUT
SLVESU	Set up equation solver by identifying fill-in positions in the Newton-Raphson matrix.	NOPCNV, NOPCNR, STORAG	INPUT GZ
SOLVE	Solve the one degree of freedom linear system of equation.		RD3DOF, RD2DOF, GENSL3, RD1DOF, GENCON
SOLVEN	Solve the $N$ degree of freedom linear system of equations.	LUBKSB LUDCMP	
SOLVE2	Solve the two degree of freedom linear system of equations.		RD3DOF, GENSL1

---



---

**TABLE III. Subroutine Calls Within FEHMN**


---

<b>Name</b>	<b>Description</b>	<b>Calls</b>	<b>Called by</b>
<b>SOLVE3</b>	Solve the three degree of freedom linear system of equations.		<b>GNSTR3, GENSL4, RD3DOF</b>
<b>STEADY</b>	Set up initial pressure distribution when gravity is present (enabled).	<b>BNSWER, ENTHP</b>	<b>GZ</b>
<b>STORAG</b>	Write out storage requirements of matrices and arrays associated with the solution of linear equations (Newton-Raphson equations).		<b>SLVESU</b>
<b>STORSX</b>	Manage the storage or retrieval of element coefficients from auxiliary file.	<b>GZ</b>	
<b>THERMC</b>	Evaluate tracer equation of state information.		<b>RDCON, CNSWER</b>
<b>THERMW</b>	Evaluate the thermodynamic properties (density, enthalpy, and viscosity) as a function of pressure and temperature (or saturation).	<b>CAPPR, POROSI RLPERM VFCAL</b>	<b>VARCHK, SOLVE</b>
<b>THRMWC</b>	Evaluate the thermodynamic properties (density, enthalpy, and viscosity) as a function of pressure, temperature and partial pressure of noncondensable gas for water/noncondensable gas problems.	<b>RLPERM CAPPR, PSAT, VFCAL</b>	<b>VARCHK</b>
<b>TIMCRL</b>	Control time step information and stopping criteria.	<b>DUAL, DISK, CO2CTR, PLOT, CONTR</b>	<b>GZ</b>
<b>TYMING</b>	Calculate CPU time for a particular computer run.	<b>SYSTEM CLOCK*</b>	<b>GZ</b>
<b>USER</b>	A user programmed subroutine that provides for changing common block variably every time step. Disabled for YMP work.		<b>GZ,INPUT</b>

---

\*Call is made to the system clock of the computer on which it is run.

---



---

**TABLE III. Subroutine Calls Within FEHMN**


---

Name	Description	Calls	Called by
<b>USERC</b>	User defined subroutine for changing common variables associated with tracer transport. Disabled for YMP project.		CONCEN
<b>VARCHK</b>	Decide, based on current pressure, temperature and saturation values current phase state (fully saturated, partially saturated). Call routine THERMW or THRMWC to update thermodynamic properties of density, enthalpy, and viscosity. Add the Newton-Ralphson corrections to the dependent variables.	THRMWC, THERMW, PSAT	GZ, BNSWER, DUAL, DUALFA
<b>VELOC</b>	Calculate velocities in coordinate directions.		GZ, CONTR
<b>VFCAL</b>	Change porosity and permeability as functions of pressure (when enabled).		THRMWC, THERMW
<b>WRTCON</b>	Write output for tracer at specified intervals.		CONCEN
<b>WRTOUT</b>	Print output information at a user specified interval.	POROSI, CO2CTR, CONCEN, SICE,	GZ
<b>ZONE</b>	Divide the input problem space by allowing the user to define zones geometrically and then labeling the nodes as to which zone they belong to. These zones are then used to assign properties to the nodes.	GENDAT, SFN3R, SFN2R, GEOIN	INPUT

---



---

## B. Common Block and Parameter Statements

The common block and parameter statements are contained in INCLUDE files. The INCLUDE files needed to compile FEHMN are COMAI, COMBI, COMCI, COMDI, COMEI, COMFI, COMGI, COMHI, COMII, COMPRI, and DAVIDI. The INCLUDE file COMDTI contain the parameter statements and will be described first. If a variable is entered, the input MACRO statement is indicated parenthetically.

### INCLUDE file COMDTI (parameter statements)

Only parameters that are different from those found in COMPRI are described.

- N0 - maximum number of nodes allowed
- N2 -  $2 * N0$ , storage parameter
- N3 -  $3 * N0$ , storage parameter
- N4 - array storage parameter for noncondensable gas solution
- N5 - array storage parameter for dual porosity solution
- N6 - array storage for ice solution
- N7 - array storage for tracer solution
- N8 - array storage for variable porosity solution
- NR - maximum space allowed for each finite element coefficient array
- NBD -  $180 * N0$  maximum array space for incomplete LU decomposition matrix
- LDN - maximum array space needed for Jacobian array matrix
- NELMD - maximum array space for element connectivity array and (later) the nodal connectivity array
- NNOP - maximum array space for LU decomposition connectivity array
- NN - maximum number of connected elements
- NQ - maximum array space for each finite element coefficient array associated with the stress solution
- NE1 - array size of common block /FE<sub>BB</sub>/,  $NELMD + NNOP + 4N0$
- NE2 - array size of common /FE<sub>B</sub>/,  $N0 + 9NR + 6NQ$
- NE3 - array size of common block /F<sub>BS</sub>/,  $3N0 + 336$
- NE5 - array size of common block / F<sub>CC</sub>/,  $39N0 + 5N7$
- NE6 - array size of common block / F<sub>DD</sub>/,  $36N0$
- NE7 - array size of common block / F<sub>DD1</sub>/,  $14N7 + 870$
- NE8 - array size of common block / F<sub>FD2</sub>/,  $7N8 + 4$
- NE9 - array size of common block / F<sub>DDI</sub>/,  $5N0 + 1$
- NE10 - array size of common block / F<sub>HH</sub>/,  $14N0$
- NE11 - array size of common block / CO<sub>2</sub>/,  $32N4 + 1$
- NE12 - array size of common block / F<sub>GG</sub>/,  $9NN + 2N3$
- NE13 - array size of common block / DUALP/,  $23N5$
- NE14 - array size of common block /FICE/ $2*N6 + 1$
- NE15 - array size of common block /ICE/ $N6$

## INCLUDE File COMAI

common/FAA/

IAB - iteration counter in stress routines  
IAC - counter for print-out interval  
IAD - current iteration number in flow solution  
IACCMX - maximum iterations allowed for time step increase (tracer solution)  
IAMM - maximum iterations allowed for time step increase (heat and mass solution)  
IAMX - iteration count after which the time step will be halved  
ICAPP - indicates capillary pressure model  
ICE - parameter which indicates if the ICE solution is enabled  
ICEN - parameter which indicates if the tracer solutions enabled  
ICF - parameter indicating status of tracer solution  
ICS - parameter indicating status of tracer solution  
ICGTS - parameter controlling the time of solution parameter changes  
ICHNG - number of thermodynamic region changes  
ICNL - indicates problem dimension  
ICO2 - indicates if noncondensable gas solution is enabled (CO2I)  
ICONTR - parameter used in contour plot management  
IDOF - number of degrees of freedom per node for the current problem  
IDUALP - parameter which indicates if the dual porosity solution is enabled (DUAL)  
IFINSH - indicates if the finishing criteria for the simulation is achieved  
IHF - parameter indicating status of flow solution (TRAC)  
IHS - parameter indicating status of flow solution (TRAC)  
III - print-out interval, number of time steps (TIME)  
IFLAG - flag used in input subroutine  
IINP - unit number input file  
ILT - parameter used in time step control  
INTG - indicates integration type used  
IPOROS - indicates if deformation model is enabled (PPOR)  
IPQZ - the number of nodes used for the contour plot output  
IPSAT - parameter regulating call to subroutine PSAT (EOS)  
IOUT - unit number for output file  
IREAD - unit number for restart file (to read)  
IREORD - parameter to reorder system of linear equations  
IRPD - indicates relative permeability model  
ISTRS - parameter indicating if the stress solution is enabled  
ISAVE - unit number for restart file (to write)  
ITER - number of iterations of last call to SOLVE(N) subroutine  
ITERT - intermediate iteration counter  
ITOTAL - total iteration count  
ITSAT - parameter specifying the setting of saturation temperature  
IYEAR - current year in simulation



**IVFCAL** - indicates if VFCAL subroutine will be called  
**IW** - number of storage locations needed to store geometric input types  
**IWELB** - indicates if wellbore solution is enabled  
**L** - current time step number  
**LDA** - parameter which specifies if the geometric coefficients are saved (CTRL)  
**M** - total number of nodes used for output information (NODE)  
**MLZ** - out of bounds node  
**MAXIT** - maximum number of iterations allowed before time step is halved (CTRL)  
**MINK** - number of active variables  
**MONTH** - current month in simulation  
**N** - total number of nodes  
**NBND** - maximum number of nonzeros per row in the incidence matrix  
**NCNTR** - contour plot interval (CONT)  
**NDEM** - coordinate direction perpendicular to the contour plane  
**NI** - number of integration points per element  
**NICG** - parameter used in time step control  
**NEI** - total number of elements in the problem (ELEM)  
**NEQ** - number of nodes, not including dual porosity nodes (CORD)  
**NEIGH** - maximum number of neighbors occur in tracer solution  
**NEMX** - number of unique (geometrically) elements  
**NORTH** - maximum number of orthogonalizations allowing in (CTRL)  
**NS** - number of nodes per element (ELEM)  
**NSAVE** - indicates if a restart file will be created in the current problem  
**NSNK** - number of source or sink terms  
**NSTEP** - maximum number of time steps

**/FAAR/**

**AIAA** - time step multiplication factor (CTRL)  
**ANO** - initial tracer concentration (TRAC)  
**AM0** - initial mass in problem  
**AMASS** - current mass in problem  
**AMP** - initial energy in system problem  
**ASTEAM** - current steam mass in problem  
**ASTM0** - initial stem mass in problem  
**AENER** - current energy in problem  
**AW** - time step weighting parameter for heat and mass solution (CTRL)  
**AWC** - time step weighting parameter (TRAC)  
**AWT** - value of implicitness factor  
**AY** - time step weighting parameter for tracer (TRAC)  
**AYC** - time step weighting parameter for tracer  
**CONTIM** - interval (days) for contour plot output  
**DAY** - current time step size in days  
**DAYCF** - time at which tracer solution stops (TRAC)  
**DAYCMM** - minimum time step size for tracer solution  
**DAYCMX** - maximum time step size for tracer solution

DAYCS - time at which tracer solution starts (TRAC)  
 DAYHF - time at which flow solution stops (TRAC)  
 DAYHS - time at which flow solution starts (TRAC)  
 DAYMAX - maximum time step allowed (CTRL)  
 DAYMIN - minimum time step allowed (CTRL)  
 DAYNEW - parameter used in time step control  
 DAYS - current simulation time  
 DAYSCN - next time for contour plot  
 DAYSI - simulation time at last time step  
 DAYSP - time at next time step  
 DEN - intermediate value of mass accumulation term  
 DENE - intermediate value of energy accumulation term  
 DEPCNG - depth at which temperature gradient changes  
 DIFE - energy balance error  
 DIFM - mass balance error  
 DITND - next time step change time  
 DNWGT - upwind weighting parameter  
 DNWGTA - upwind weighting parameter in tracer solution  
 DTOT - current time step size in seconds  
 DTOTC - tracer time step size in seconds  
 DTOTDM - last time step size in seconds  
 EPC - specified solution tolerance for tracer solution  
 EPE - tolerance for Newton-Raphson iteration  
 EPS - tolerance for linear equation solver  
 F0 - initial time step residual  
 FDUM - current sum squared of residuals  
 GRAD2 - parameter in description of temperature gradient  
 GRADNT - parameter used in description of temperature gradient  
 GRAV - value of gravity  
 G1 - iteration accuracy control parameter (ITER)  
 G2 - iteration accuracy control parameter (ITER)  
 G3 - iteration accuracy control parameter (ITER)  
 OVERF - over relaxation factor for SOR equations (ITER)  
 PEIN - initial pressure of problem (INIT)  
 POW - power output for a given time step  
 QT - total outflow for time step  
 QTE - total energy outflow for time step  
 QTOT - total outflow for problem  
 QTOTE - total energy outflow for problem  
 QTOTEI - intermediate energy flow total  
 QTOTI - intermediate flow total  
 QUAD - parameter used in temperature gradient  
 RNMAX - maximum run time allowed  
 SECMA - maximum time step size in seconds

**STR** - multiplier for Newton-Raphson corrections  
**STRD** - multiplier for Newton-Raphson corrections  
**SV** - vapor saturation of a node  
**SW** - liquid saturation of a node  
**TEOUTF** - parameter used in calculation of energy output  
**TIMS** - ending simulation time (TIME)  
**TIN** - parameter used in temperature gradient  
**TIN0** - initial problem temperature (INIT)  
**TIN1** - parameter used in temperature gradient  
**TMCH** - machine tolerance (ITER)  
**TOUTFL** - parameter used in calculation of flow output  
**UPWGT** - upwind weighting parameter  
**UPWGTA** - upwind weighting factor for tracer solution (TRAC)  
**UPWGTB** - upwind weighting factor for tracer solution  
**VLMAX** - maximum liquid phase velocity  
**VTOT** - total volume in problem  
**VVMAX** - maximum vapor phase velocity

**common/FAAC/**

**SSSOL** - indicates if initial steady state solution is needed  
**VEQNO** - contains version number of FEHMN code used

**common/FAAC1/**

**IDATE** - contains the date (mm/dd/yr)

**INCLUDE file COMBI**

**common/FBB/**

**NELM(NELMD)** - initially information about nodes in each element, later nodal connectivity information  
**NOP(NNOP)** - matrix sparsity structure for LU decomposition  
**NAR(N0)** - array containing gauss elimination order for each node  
**ISTRW(N0)** - starting positions in sx(nr,9) array of finite element coefficients for each node  
**KA(N0)** - contains boundary type information for each node  
**NELMDG(N0)** - contains position of (i,i) element in connectivity array

### **common/FBC/**

- SX1(N0)** - contains volume associated with each node
- SX(NR,9)** - contains finite element geometric coefficients necessary for heat and mass transfer simulation
- SXS(NQ,6)** - contains more finite element geometric coefficients (ie., those necessary for the stress module)

### **common/FBS/**

- CORD(N0,3)** - contains the coordinates of each node
- XD(8),YD(8),ZD(8)** - global coordinates of the nodes in a finite element
- SI(8),ETA(8),EXCI(8)** - local coordinates in a finite element of the numerical integration points
- XT(8),YT(8),ZT(8)** - parameters needed in element calculations
- W(8,8)** - finite element shape functions
- WX(8,8)** - derivative of shape functions with respect to x
- WY(8,8)** - derivative of shape functions with respect to y
- WZ(8,8)** - derivative of shape functions with respect to z
- DR(8)** - contains weights for integration points (bricks, rectangles)
- DP(6)** - contains weights for integration points (prisms, triangles)
- WR(8,8)** - finite element shape functions (rectangles)
- WXR(8,8)** - derivative of shape functions with respect to x (rectangles)
- WYR(8,8)** - derivative of shape functions with respect to y (rectangles)
- WZR(8,8)** - derivative of shape functions with respect to z (rectangles)
- WP(8,8)** - finite element shape functions (prisms)
- WXP(8,8)** - derivative of shape functions with respect to x (prisms)
- WYP(8,8)** - derivative of shape functions with respect to y (prisms)
- WZP(8,8)** - derivative of shape functions with respect to z (prisms)

### **INCLUDE File COMCI**

### **common/FCC/**

- DANL(N7)** - derivative of liquid phase concentration with respect to total concentration
- DANV(N7)** - derivative of vapor phase concentration with respect to total concentration
- AKC(N7)** - tracer accumulation term derivative with respect to total concentration
- DRC(N7)** - tracer source term derivative with respect to total concentration
- DEEF(N0)** - derivative of energy accumulation with respect to energy variable
- DEPF(N0)** - derivative of energy accumulation term with respect to pressure

DMPF(N0) - derivative of mass accumulation term with respect to pressure  
 DMEF(N0) - derivative of mass accumulation term with respect to energy variable  
 DQ(N0) - derivative of mass source term with respect to pressure  
 DQH(N0) - derivative of energy source term with respect to pressure  
 DEQH(N0) - derivative of energy source term with respect to energy variable  
 DTPAE(N0) - derivative of temperature with respect to energy variable  
 DTPA(N0) - derivative of temperature with respect to pressure  
 DEVEF(N0) - derivative of enthalpy with respect to energy variable  
 DEVF(N0) - derivative of enthalpy with respect to pressure  
 DRVPF(N0) - derivative of vapor relative permeability with respect to pressure  
 DRVEF(N0) - derivative of vapor relative permeability with respect to energy variable  
 DGLE(N0) - derivative of liquid mass gravity term with respect to energy variable  
 DGLP(N0) - derivative of liquid mass gravity term with respect to pressure  
 DELEF(N0) - derivative of liquid enthalpy with respect to energy variable  
 DELF(N0) - derivative of liquid enthalpy with respect to pressure  
 DRLPF(N0) - derivative of liquid relative permeability with respect to pressure  
 DRLEF(N0) - derivative of liquid relative permeability with respect to energy variable  
 DILE(N0) - derivative of liquid transmissibility with respect to energy variable  
 DILP(N0) - derivative of liquid transmissibility with respect to pressure  
 ENLF(N0) - liquid enthalpy  
 ENVF(N0) - vapor enthalpy  
 DSTM(N0) - steam mass  
 DENI(N0) - mass accumulation term  
 DENEI(N0) - energy accumulation term  
 DIL(N0) - liquid transmissibility  
 DIV(N0) - vapor transmissibility  
 ROLF(N0) - liquid density  
 ROVF(N0) - vapor density  
 RLF(N0) - liquid phase relative permeability  
 RVF(N0) - vapor phase relative permeability  
 DENC1(N7) - tracer accumulation term  
 GL(N0) - liquid phase gravity term  
 GV(N0) - vapor phase gravity term  
 DIVE(N0) - derivative of vapor transmissibility with respect to energy variable  
 DIVP(N0) - derivative of vapor transmissibility with respect to pressure  
 DGVP(N0) - derivative of vapor mass gravity term with respect to pressure  
 DGVE(N0) - derivative of vapor mass gravity term with respect to energy variable  
 DPCEF(N0) - derivative of capillary pressure with respect to the energy variable

**INCLUDE file COMDI**

**common/FDD/**

THX(N0) - thermal conductivity x-direction

THY(N0) - thermal conductivity y-direction  
 THZ(N0) - thermal conductivity z-direction  
 VOLUME(N0) - volume associated at each node  
 SK(N0) - source strength of each node  
 ESK(N0) - inlet enthalpy associated with a source  
 QFLUX(N0) - heat flux at each node  
 QFLXM(N0) - heat flux impedance at each node  
 PNX(N3) - permeability in the x-direction, liquid velocity in the x-direction,  
 vapor velocity in the x-direction  
 PNY(N3) - permeability in the y-direction, liquid velocity in the y-direction,  
 vapor velocity in the y-direction  
 PNZ(N3) - permeability in the z-direction, liquid velocity in the z-direction,  
 vapor velocity in the z-direction  
 PS(N0) - porosity at each node  
 EFLOW(N0) - energy flow at each source node  
 PHI(N0) - pressure at each node  
 PHO(N0) - last time step pressure at each node  
 T(N0) - temperature at each node  
 TO(N0) - last time step pressure at each node  
 VF(N0) - volume factor at each node  
 PFLOW(N0) - flowing pressure at each source node  
 DENEH(N0) - last time step energy accumulation term at each node  
 QH(N0) - energy source term at each node  
 S(N0) - liquid saturation at each node  
 SO(N0) - last time step saturation at each node  
 WELLIM(N0) - well impedance at each source node  
 DENH(N0) - last time step mass accumulation term at each node  
 DENJ(N0) - last time step mass accumulation time derivative at each node  
 DENEJ(N0) - last time step energy accumulation time derivative at each node  
 DENR(N0) - rock density at each node  
 CPR(N0) - rock specific heat at each node  
 PCP(N0) - capillary pressure at each node

**common/FDDI/**

NSKW(N0) - contains nodes for print-out

**common/FDD1/**

AN(N7) - total tracer concentration at each node  
 ANL(N7) - liquid tracer concentration at each node  
 ANV(N7) - vapor tracer concentration at each node  
 CNSK(N7) - tracer concentration source term at each node

**T1SK(N7)** - time when the tracer source term is activated at each node  
**T2SK(N7)** - time when the tracer source term is terminated at each node  
**RC(N7)** - tracer source term at each node  
**DENCH(N7)** - last time step tracer accumulation term at each node  
**DENCJ(N7)** - last time step tracer accumulation derivative term at each node  
**ANLO(N7)** - last time step total tracer concentration at each node  
**FC(N7)** - tracer equation residual at each node  
**TCX(N7)** - tracer diffusion term in the x-direction  
**TCY(N7)** - tracer diffusion term in the y-direction  
**TCZ(N7)** - tracer diffusion term in the z-direction  
**CM(10)** - total tracer mass for each specie  
**CM0(10)** - initial total tracer mass for each specie  
**QCIN(10)** - total injected tracer mass for each specie  
**QOUT(10)** - total produced tracer mass for each specie  
**A1ADF(10)** - alpha1 parameter for each specie (nonlinear adsorption)  
**A2ADF(10)** - alpha2 parameter for each specie (nonlinear adsorption)  
**BETADF(10)** - beta parameter for each specie (nonlinear adsorption)  
**A1R** - parameter in reaction rate model  
**A2R** - parameter in reaction rate model  
**A3R** - parameter in reaction rate model  
**A4R** - parameter in reaction rate model  
**RP1F(25)** - parameter in relative permeability model  
**RP2F(25)** - parameter in relative permeability model  
**RP3F(25)** - parameter in relative permeability model  
**RP4F(25)** - parameter in relative permeability model  
**RP5F(25)** - parameter in relative permeability model  
**RP6F(25)** - parameter in relative permeability model  
**RP7F(25)** - parameter in relative permeability model  
**RP8F(25)** - parameter in relative permeability model  
**RP9F(25)** - parameter in relative permeability model  
**RP10F(25)** - parameter in relative permeability model  
**RP11F(25)** - parameter in relative permeability model  
**RP12F(25)** - parameter in relative permeability model  
**RP13F(25)** - parameter in relative permeability model  
**RP14F(25)** - parameter in relative permeability model  
**RP15F(25)** - parameter in relative permeability model  
**RP16F(25)** - parameter in relative permeability model  
**RP17F(25)** - parameter in relative permeability model  
**CP1F(10)** - parameter in capillary pressure model  
**CP2F(10)** - parameter in capillary pressure model  
**CP3F(10)** - parameter in capillary pressure model  
**DIT(300)** - array containing time step changes

### **common/FDD1I/**

NSPECI - number of species for tracer solution  
NSP - current specie number  
NPN - parameter used in storing tracer data  
NPT(10) - storage parameter used in tracer solution  
IADD(10) - iteration count for tracer solution  
IADDT(10) - iteration count used for linear equation solver in tracer solution  
IADSF(10) - adsorption model used in tracer solution  
ICAPT(10) - capillary pressure model  
IRLPT(10) - relative permeability model  
ICNS(10) - liquid or gas phase tracer model  
ICRATE - reaction rate model  
ITC(100) - array containing information used in time step changes

### **common/FDD2/**

PHINI(N8) - initial pressure at each node  
PSINI(N8) - initial porosity at each node  
DPORP(N8) - derivative of porosity with respect to pressure at each node  
DPORT(N8) - derivative of porosity with respect to temperature at each node  
TINI(N8) - initial temperature at each node  
SIGINI - parameter used in rock deformation model  
PHYDRO - parameter used in rock deformation model  
THEXP - parameter used in rock deformation model  
YOUNG - parameter used in rock deformation model  
AMGANG(N8) - parameter used in gangi model at each node  
PGANGI(N8) - parameter used in gangi model at each node

### **common/FICE/**

SII(N6) - ice saturation at each node  
SIO(N6) - last time step value of ice saturation  
TMELT - freezing temperature of water



**common/IICE/**

- ICES(N6) - state of ice at each node
  
- IIEOS(N0) - thermodynamics set at each node
- IEOS(N0) - phase state of fluid at each node
- IEOSC - phase change parameter
- IPORF(N0) - deformation model at each node
- IRLP(N0) - relative permeability model at each node
- ICAP(N0) - capillary pressure model at each node

**INCLUDE file COMEI**

**common/FEE/**

- A(LDN) - array containing the Jacobian matrix

**common/FFF/**

- B(NBD) - array containing the incomplete LU decomposition of the Jacobian matrix

**common/FHH/**

- IRB(N0) - array containing the reordered node numbers
- IIRB(N0) - inverse of irb
- NOPT(N0) - array indicating active variables
- NPVT(N0) - pivot information for the LU decomposition matrix
- IG(N0) - variable order LU decomposition information
- PIV(N0,9) - the pivot elements of the LU decomposition

**INCLUDE file COMFI**

- DMC(N4) - derivative of mass accumulation term with respect to gas at each node
- DEC(N4) - derivative of energy accumulation term with respect to gas at each node
- DCP(N4) - derivative of gas accumulation term with respect to pressure at each node
- DCE(N4) - derivative of gas accumulation term with respect to energy at each node
- DQC(N4) - derivative of mass source term with respect to gas
- DEQC(N4) - derivative of energy source term with respect to gas
- DCQC(N4) - derivative of gas source term with respect to gas

DENPCI(N4) - gas accumulation term at each node  
 DENPCH(N4) - last time step value of the mass accumulation term at each node  
 DIVC(N4) - derivative of vapor transmissibility with respect to gas  
 DGVC(N4) - derivative of vapor gravity term with respect to gas  
 DCVCF(N4) - derivative of gas concentration with respect to gas  
 DCVEF(N4) - derivative of gas concentration with respect to energy  
 DCVF(N4) - derivative of gas concentration with respect to pressure  
 DEVCF(N4) - derivative of energy with respect to gas  
 CNVF(N4) - concentration of gas in the vapor phase  
 DILC(N4) - derivative of liquid transmissibility with respect to gas  
 DGLC(N4) - derivative of liquid gravity term with respect to gas  
 ESKC(N4) - source term for gas equation  
 DCLCF(N4) - derivative of liquid concentration with respect to gas  
 DCLEF(N4) - derivative of liquid concentration with respect to energy  
 DCLF(N4) - derivative of liquid concentration with respect to pressure  
 DELCF(N4) - derivative of liquid energy with respect to gas  
 CNLF(N4) - gas concentration in the liquid phase  
 QC(N4) - source term for the gas equation  
 DCC(N4) - derivative of gas accumulation term with respect to gas  
 DTPAC(N4) - derivative of temperature with respect to gas  
 DENPCJ(N4) - last time step accumulation term of gas equation  
 DCQH(N4) - derivative of gas source term with respect to energy  
 PCI(N4) - gas pressure  
 PCIO(N4) - last time step gas pressure  
 DIFC - noncondensable gas mass balance error

## INCLUDE file COMGI

### common/FGG/

DFMP(NN) - derivative of mass accumulation term with respect to pressure for neighbor nodes  
 DFME(NN) - derivative of mass accumulation term with respect to energy for neighbor nodes  
 DFEP(NN) - derivative of energy accumulation term with respect to pressure for neighbor nodes  
 DFEE(NN) - derivative of energy accumulation term with respect to energy for neighbor nodes  
 DFMP(NN) - derivative of mass accumulation term with respect to gas for neighbor nodes  
 DFEP(NN) - derivative of energy accumulation term with respect to gas for neighbor nodes  
 DFPCP(NN) - derivative of gas accumulation term with respect to pressure for neighbor nodes  
 DFPCE(NN) - derivative of gas accumulation term with respect to energy for

- neighbor nodes
- DFPCPC(NN) - derivative of gas accumulation term with respect to gas for neighbor nodes
- BP(N3) - array of Newton-Raphson residuals, after solution, an array of Newton-Raphson corrections
- BPC(N3) - array of Newton-Raphson residuals for gas, after solution, an array of Newton-Raphson corrections

**INCLUDE file COMHI**

**common/DUALP/**

- VOLF1(N5) - volume fraction at each node for the first matrix layer
- VOLF2(N5) - volume fraction at each node for the second matrix layer
- APUV1(N5) - area per unit volume for the first matrix layer
- WB11(N5) - array needed to store intermediate dual porosity results
- WB12(N5) - array needed to store intermediate dual porosity results
- WB21(N5) - array needed to store intermediate dual porosity results
- WB22(N5) - array needed to store intermediate dual porosity results
- TB11(N5) - array needed to store intermediate dual porosity results
- TB12(N5) - array needed to store intermediate dual porosity results
- TB21(N5) - array needed to store intermediate dual porosity results
- TB22(N5) - array needed to store intermediate dual porosity results
- A21MPF(N5) - array needed to store intermediate dual porosity results
- A21MEF(N5) - array needed to store intermediate dual porosity results
- A21EPF(N5) - array needed to store intermediate dual porosity results
- A21EEF(N5) - array needed to store intermediate dual porosity results
- A32MPF(N5) - array needed to store intermediate dual porosity results
- A32MEF(N5) - array needed to store intermediate dual porosity results
- A32EPF(N5) - array needed to store intermediate dual porosity results
- A32EEF(N5) - array needed to store intermediate dual porosity results
- RB2MF(N5) - array needed to store intermediate dual porosity results
- RB2EF(N5) - array needed to store intermediate dual porosity results
- RB3MF(N5) - array needed to store intermediate dual porosity results
- RB3EF(N5) - array needed to store intermediate dual porosity results

**INCLUDE file COMII**

**common/COEFF/**

- CEL(20,2) - polynomial coefficients for liquid water enthalpy equations
- CRL(20,2) - polynomial coefficients for liquid water density equations
- CEV(20,2) - polynomial coefficients for vapor water enthalpy equations

- CRV(20,2) - polynomial coefficients for vapor water density equations
- CVL(20,2) - polynomial coefficients for liquid water viscosity equations
- CVV(20,2) - polynomial coefficients for vapor water viscosity equations
- TSA0 - polynomial coefficient for saturation temperature equation
- TSPA1 - polynomial coefficient for saturation temperature equation
- TSPA2 - polynomial coefficient for saturation temperature equation
- TSPA3 - polynomial coefficient for saturation temperature equation
- TSPA4 - polynomial coefficient for saturation temperature equation
- TSB0 - polynomial coefficient for saturation temperature equation
- TSPB1 - polynomial coefficient for saturation temperature equation
- TSPB2 - polynomial coefficient for saturation temperature equation
- TSPB3 - polynomial coefficient for saturation temperature equation
- TSPB4 - polynomial coefficient for saturation temperature equation
- PSA0 - polynomial coefficient for saturation pressure equation
- PSTA1 - polynomial coefficient for saturation pressure equation
- PSTA2 - polynomial coefficient for saturation pressure equation
- PSTA3 - polynomial coefficient for saturation pressure equation
- PSTA4 - polynomial coefficient for saturation pressure equation
- PSB0 - polynomial coefficient for saturation pressure equation
- PSTB1 - polynomial coefficient for saturation pressure equation
- PSTB2 - polynomial coefficient for saturation pressure equation
- PSTB3 - polynomial coefficient for saturation pressure equation
- PSTB4 - polynomial coefficient for saturation pressure equation

**common/COEFF1/**

- PMAX(3) - maximum pressure allowed for each coefficient set
- PMIN(3) - minimum pressure allowed for each coefficient set
- TMAX(3) - maximum temperature allowed for each coefficient set
- TMIN(3) - minimum temperature allowed for each coefficient set

**common/COEFF2/**

- EW1 - coefficient used in simplifying thermodynamics relations
- EW2 - coefficient used in simplifying thermodynamics relations
- EW3 - coefficient used in simplifying thermodynamics relations
- EW4 - coefficient used in simplifying thermodynamics relations
- EW5 - coefficient used in simplifying thermodynamics relations
- EW6 - coefficient used in simplifying thermodynamics relations
- EW7 - coefficient used in simplifying thermodynamics relations
- EW8 - coefficient used in simplifying thermodynamics relations
- EW9 - coefficient used in simplifying thermodynamics relations
- EW10 - coefficient used in simplifying thermodynamics relations
- EW11 - coefficient used in simplifying thermodynamics relations

- EV1 - coefficient used in simplifying thermodynamics relations
- EV2 - coefficient used in simplifying thermodynamics relations
- EV3 - coefficient used in simplifying thermodynamics relations
- EV4 - coefficient used in simplifying thermodynamics relations
- EV5 - coefficient used in simplifying thermodynamics relations
- EV6 - coefficient used in simplifying thermodynamics relations
- EV7 - coefficient used in simplifying thermodynamics relations
- EV8 - coefficient used in simplifying thermodynamics relations
- EV9 - coefficient used in simplifying thermodynamics relations
- EV10 - coefficient used in simplifying thermodynamics relations
- EV11 - coefficient used in simplifying thermodynamics relations

**INCLUDE file DAVIDI**

**common/DAVID1/**

- IRDOF - reduced degree of freedom model used
- ISLORD - parameter used in the reduced degree of freedom model
- IBACK - LU factorization save parameter
- ICOUPL - number of SOR iterations
- ITEST - parameter used in the reduced degree of freedom model

**common/DAVID2/**

- NMAT(9) - array used in the reduced degree of freedom method
- NRHS(3) - array used in the reduced degree of freedom method
- NMAT32(4) - array used in the reduced degree of freedom method

**C. Subroutine Structure for FEHMN**

Figure 4 presents the general subroutine call tree structure for the code FEHMN. Due to its complexity, the entire structure could not fit within a page, hence it is broken into several branches. As an example of the tree's use we trace the call structure from GZ (the main program), which calls INPUT (0003), which calls CONCEN(0021), which calls CSOLVE (0026), which calls CNSWER (0028) which calls THERMC (0028). At subroutine THERMC, the tree is directed to line 0024 where the calls from THERMC have been previously explained. We see that THERMC calls DABS. This was only one path of many possible; all paths may be traversed in a way analogous to above.

```

0001 6Z-----+---TYMING-----#CLOCK
0002          +---DATA
0003          +---INPUT-----+---IOFILE
0004          |               +---#IABS
0005          |               +---#MAXO
0006          |               +---#THER
0007          |               +---#GEOIN
0008          |               +---#USER
0009          |               +---#ZONE-----+---#GEOIN
0010          |               |               +---#IABS
0011          |               |               +---#GENDAT
0012          |               |               +---#SFN3R
0013          |               |               +---#SQRT
0014          |               |               +---#ABS
0015          |               |               +---#SFN2R
0016          |               +---#POROSI-----+---#IABS
0017          |               |               +---#MAXO
0018          |               |               +---#ROCK-----+---#MAXO
0019          |               +---#DABS
0020          |               +---#GENDAT
0021          |               +---#CONCEN-----+---#RDCON-----+---#DMIN1
0022          |               |               |               +---#MAXO
0023          |               |               |               +---#IABS
0024          |               |               |               +---#THERMC-----+---#DABS
0025          |               |               |               +---#PLOT1
0026          |               |               +---#CSOLVE-----+---#DMIN1
0027          |               |               |               +---#DABS
0028          |               |               |               +---#CMSVER-----+---#THERMC-----> 0024
0029          |               |               |               |               +---#GENCOM-----+---#CONEQ1
0030          |               |               |               |               +---#DSQRT
0031          |               |               |               |               +---#DMAX1
0032          |               |               |               |               +---#DMIN1
0033          |               |               |               |               +---#SOLVE-----+---#DSQRT
0034          |               |               |               |               |               +---#DMAX1
0035          |               |               |               |               |               +---#DABS
0036          |               |               |               |               +---#RD1DOF-----+---#DSQRT
0037          |               |               |               |               |               +---#SOLVE-----> 0033
0038          |               |               |               |               +---#THERMC-----> 0024
0039          |               |               |               |               +---#PLOT1
0040          |               |               +---#WRTCON-----+---#DABS
0041          |               |               +---#DISK
0042          |               |               +---#CONTRC
0043          |               +---#STRESS
0044          |               +---#CO2CTR-----+---#MAXO
0045          |               |               +---#IABS
0046          |               |               +---#PSAT-----+---#DABS
0047          |               |               +---#DABS
0048          |               +---#DUAL-----+---#VARCHK-----+---#MAXO
0049          |               |               |               +---#PSAT-----> 0046
0050          |               |               |               +---#DABS
0051          |               |               |               +---#THRNV-----+---#RLPERM-----+---#IABS
0052          |               |               |               |               |               +---#MAXO
0053          |               |               |               |               |               +---#DSQRT
0054          |               |               |               |               +---#CAPPR-----+---#IABS
0055          |               |               |               |               |               +---#MAXO
0056          |               |               |               |               +---#PSAT-----> 0046
0057          |               |               |               |               +---#VFCAL-----+---#DLOG
0058          |               |               |               |               |               +---#DEXP
0059          |               |               |               +---#THERMV-----+---#RLPERM-----> 0051
0060          |               |               |               +---#POROSI-----> 0016
0061          |               |               |               +---#CAPPR-----> 0054
0062          |               |               |               +---#VFCAL-----> 0057
0063          |               |               +---#DMAX1
0064          |               +---#DUALFA-----+---#VARCHK-----> 0048
0065          |               |               +---#GENEQ1
0066          |               |               +---#GENEQ3

```

Fig. 4. Structure for subroutine calls for FEHMN.

```

0067      !           !           !           +-#BALI
0068      !           !           !           +-#BALM
0069      !           !           !           +-#DUALEX-----#ALM
0070      !           +-#CAPPR-----> 0054
0071      !           +-#RLPERM-----> 0051
0072      !           +-#SICE-----+-#IABS
0073      !           !           +-#MAXO
0074      !           !           +-#STNER
0075      !           +-#WELBOR
0076      +-#MAXO
0077      +-#NEAR3-----#DSQRT
0078      +-#CONTR-----+-#VELOC-----+-#DSQRT
0079      !           !           +-#DMAX1
0080      !           !           +-#DABS
0081      !           +-#CONCEN-----> 0021
0082      +-#ANONP-----+-#DSQRT
0083      !           +-#BTP
0084      !           +-#BAL
0085      !           +-#DABS
0086      !           +-#BVP
0087      !           +-#IABS
0088      !           +-#MAXO
0089      !           +-#GENCOF-----+-#GNCF3-----+-#SHAP3R-----#DSQRT
0090      !           !           +-#SHAP3P
0091      !           +-#GNCF2-----+-#SHAP2R-----#DSQRT
0092      +-#STORSX
0093      +-#DABS
0094      +-#DISK-----+-#CONCEN-----> 0021
0095      !           +-#STRESS
0096      +-#PEINT-----+-#DABS
0097      !           +-#DMAX1
0098      +-#RARNG
0099      +-#RADIUS
0100      +-#SLVESU-----+-#NOPCNV-----+-#MAXO
0101      !           !           +-#MINO
0102      !           +-#NOPCNR-----+-#MAXO
0103      !           !           +-#MINO
0104      !           +-#STORAG-----+-#MINO
0105      +-#SETORD
0106      +-#DUAL-----> 0048
0107      +-#CO2CTR-----> 0044
0108      +-#COEFFC
0109      +-#SICE-----> 0072
0110      +-#VARCHK-----> 0048
0111      +-#STEADY-----+-#DABS
0112      !           +-#ENTHP
0113      !           +-#BNSVER-----+-#VARCHK-----> 0048
0114      !           +-#OUTBND
0115      !           +-#GENSL3-----+-#GENEQ3
0116      !           !           +-#DSQRT
0117      !           !           +-#DMAX1
0118      !           !           +-#DMIN1
0119      !           !           +-#SOLVE-----> 0033
0120      !           !           +-#RD1DOF-----> 0036
0121      !           +-#GENSL4-----+-#GENEQC
0122      !           !           +-#GENEQ3
0123      !           !           +-#DUAL-----> 0048
0124      !           !           +-#NORMAL-----+-#BALI
0125      !           !           !           +-#BALM
0126      !           !           !           +-#BALI3
0127      !           !           !           +-#BALM3
0128      !           !           !           +-#DSQRT
0129      !           !           !           +-#DMAX1
0130      !           !           !           +-#DMIN1
0131      !           !           !           +-#SOLVE3-----+-#DSQRT
0132      !           !           !           !           +-#BALI

```

Fig. 4. (Continued)

```

0133      |           |           |           |           +-#BALM
0134      |           |           |           |           +-#DMAX1
0135      |           |           |           |           +-#DABS
0136      |           |           |           |           +-#RD3DOF---+-#SOLVE2---+-#DSORT
0137      |           |           |           |           |           +-#BALI
0138      |           |           |           |           |           +-#BALM
0139      |           |           |           |           |           +-#DMAX1
0140      |           |           |           |           |           +-#DABS
0141      |           |           |           |           |           +-#SOLVE-----> 0033
0142      |           |           |           |           |           +-#GENSL1---+-#GENEQ1
0143      |           |           |           |           |           +-#GENEQ3
0144      |           |           |           |           |           +-#DUAL-----> 0048
0145      |           |           |           |           |           +-#NORMAL-----> 0124
0146      |           |           |           |           |           +-#DSORT
0147      |           |           |           |           |           +-#DMAX1
0148      |           |           |           |           |           +-#DMIN1
0149      |           |           |           |           |           +-#SOLVE2-----> 0136
0150      |           |           |           |           |           +-#RD2DOF---+-#SOLVE-----> 0033
0151      |           |           |           |           |           +-#DSORT
0152      |           |           |           |           |           +-#CONCEN-----> 0021
0153      |           |           |           |           |           +-#PLOT
0154      |           |           |           |           |           +-#DATCHK---+-#DMIN1
0155      |           |           |           |           |           |           +-#DMAX1
0156      |           |           |           |           |           +-#TIMCRL---+-#DUAL-----> 0048
0157      |           |           |           |           |           |           +-#DISK-----> 0094
0158      |           |           |           |           |           |           +-#CO2CTR-----> 0044
0159      |           |           |           |           |           |           +-#PLOT
0160      |           |           |           |           |           |           +-#CONTR-----> 0078
0161      |           |           |           |           |           |           +-#ABS
0162      |           |           |           |           |           +-#USER
0163      |           |           |           |           |           +-#VELBOR
0164      |           |           |           |           |           +-#ENTHP
0165      |           |           |           |           |           +-#BNSVR-----> 0113
0166      |           |           |           |           |           +-#RESETV
0167      |           |           |           |           |           +-#STRESS
0168      |           |           |           |           |           +-#VELOC-----> 0078
0169      |           |           |           |           |           +-#DMAX1
0170      |           |           |           |           |           +-#VRTOUT---+-#MAXO
0171      |           |           |           |           |           |           +-#DFLOAT
0172      |           |           |           |           |           |           +-#POROSI-----> 0016
0173      |           |           |           |           |           |           +-#CO2CTR-----> 0044
0174      |           |           |           |           |           |           +-#CONCEN-----> 0021
0175      |           |           |           |           |           |           +-#STRESS
0176      |           |           |           |           |           |           +-#SICE-----> 0072
0177      |           |           |           |           |           +-#MOD

```

Fig. 4. (Continued)



### III. USER'S MANUAL

This section provides the instructions necessary for using the code FEHMN. Section A describes an automatic mesh generation code, GENMSH, that can be used to generate the finite element mesh input required by FEHMN. Section B describes in detail the input macro-commands for FEHMN. A graphics postprocessor is described in Section C and several example problems are given in Section D.

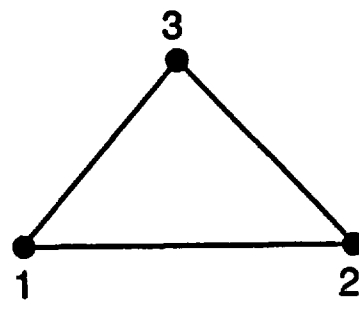
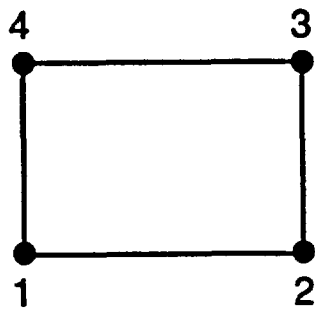
#### A. Automatic Mesh Generation

The code GENMSH, which is designed to be used in conjunction with the finite element code FEHMN, operates by dividing a user-defined solution space into a prescribed number of finite elements. The solution space may be either two or three dimensional. In order to simplify geometric considerations, the solution space is broken up into a number of "blocks." Each block is then further divided into "elements." A given block uses the same "type" of element throughout, although the elements need not be of the same size. Different blocks may use different types of elements. The choice of elements available in two dimensions for output to FEHMN are 4-noded quadrilaterals and 3-noded triangles. In three dimensions, the choice is 8-noded quadrilateral polyhedrons or 3-noded triangular prisms, shown schematically in Fig. 5.

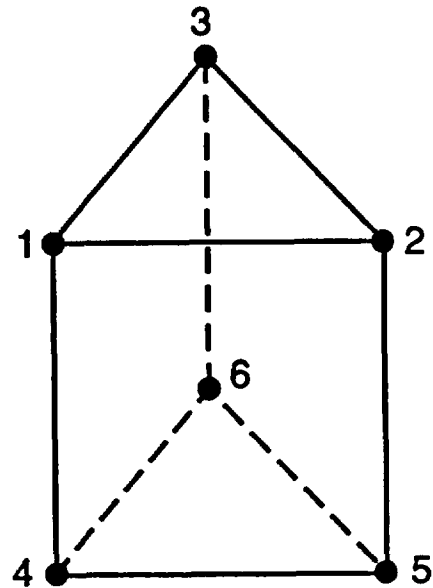
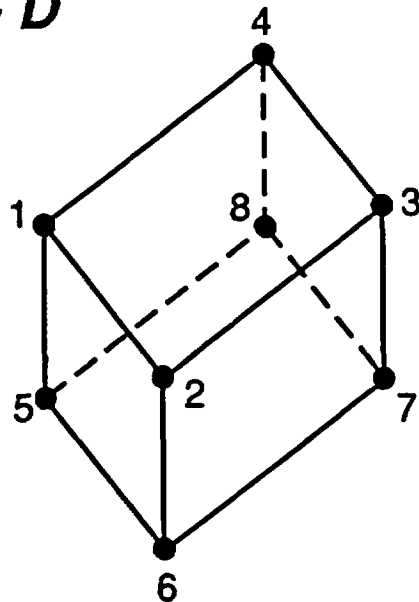
The solution space, and each block, is defined by giving the corner and/or midpoint nodes. This amounts to specifying 4 or 8 nodes per block in 2-D problems and 8 or 20 nodes per block in 3-D problems as shown in Fig. 6. The same block definition is needed for both quadrilateral and triangular elements. After discretizing the solution space and the blocks, it is necessary to specify the desired division of each block into elements. This is done by specifying the relative weights of each subdivision in each direction for each block. The reader is referred to *An Introduction to Finite Element Computations* by Hinton and Owen (pp. 328-346) for the details of the procedure and the algorithm. Note that material properties are specified at each node in FEHMN, unlike conventional finite element procedure.

A detailed description of the input to the code follows. The input must be placed in a file called MDAT. Examples of the MDAT file are given in Section D. The output is found on a file called GEOM.DAT. The output consists of a list of nodal coordinates and elements in a suitable format for the code FEHMN. Free format is used for the input. In addition, a zone definition of the input blocks is provided in file ZONE. The files GEOM.DAT and

## 2 - D

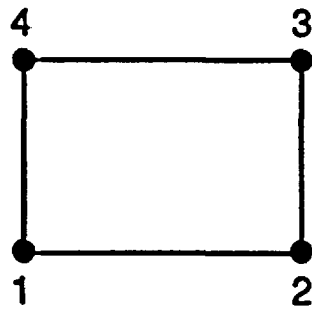


## 3 - D

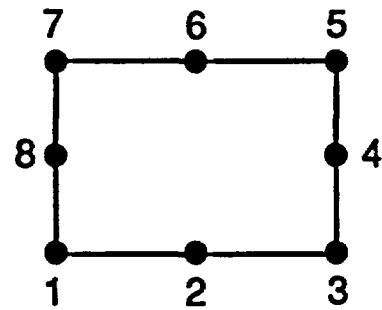


**Fig. 5.** Elements available with FEHMN in 2-D and 3-D problems showing numbering convention.

## 2 - D

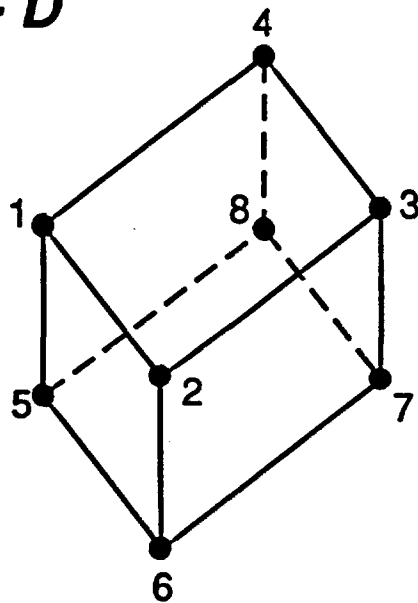


4 - node

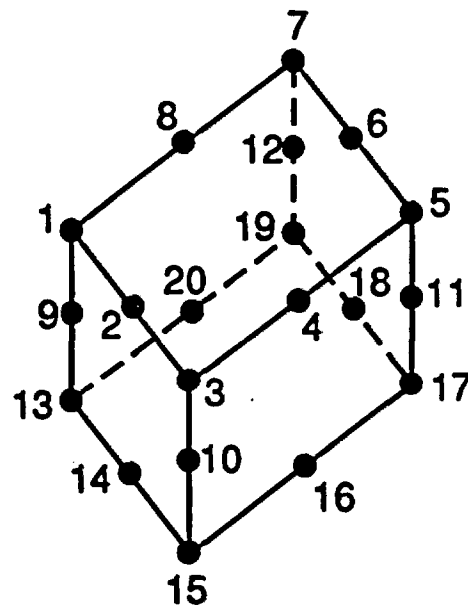


8 - node

## 3 - D



8 - node



20 - node

Fig. 6. Nodal ordering for defining 2-D and 3-D domain blocks for input to GENMSH.

ZONE may be used directly in the input file for FEHMN as they already include the appropriate macro command headings.

Group 1

Title, up to 80 characters long

Group 2

NPOIN, NELEM, LNODE, IT, NDIME, KF, NRN

NPOIN - total number of points used to define the solution space

NELEM - number of blocks used to define the solution domain

LNODE - number of nodes per block used to define the solution domain

IT - element triangulation parameter, if IT=0, then no element splitting occurs, if IT $\neq$  0, then triangle elements are generated in 2-D and prism elements are generated in 3-D.

NDIMB - dimension of problem (2 or 3)

KF - determines the vertical axis direction in 2-D. If KF < 0 then the y-axis is positive downward. If KF  $\geq$  0, the y-axis is positive upward in 3-D, the z-axis is always positive upward. See note on plotting below.

NRN - renumber parameter. If NRN  $\neq$  0 the code will renumber to minimize the band width. If NRN = 0 then no renumbering will occur.

Group 3 (NUMEL, Block Times)

NUMEL, (LNODS(NUMEL,INOD), INODE = 1, LNODE)

NUMEL - Block number

LNODS (NUMEL, INOD) - LNODE nodes defining the block NUMEL

Group 4

CORDX (I), I = 1, NPOIN

CORDX (I) - x-coordinates of points used to define the solution space

Group 5

CORDY (I), I = 1, NPOIN

CORDY (I) - y-coordinates of points used to define the solution space

Group 6 (only if NDIME = 3)

CORDZ (I), I = 1, NPOIN

CORDZ (I) - z-coordinates of points used to define the solution space

NOTE: Groups 7-10 are repeated for each block.

Group 7

KBLOC, NDIVX, NDIVY, NDIVZ

KBLOC - block number

NDIVX - number of divisions in x-direction

NDIVY - number of divisions in y-direction

NDIVZ - number of divisions in z-direction (only if NDIME = 3).

NOTE: The number of nodes in a direction = number of divisions + 1.

Group 8

WEITX (I), I = 1, NDIVX

WEITX (I) - weighting of the Ith division in the x-direction in block KBLOC

Group 9

WEITY (I), I = 1, NDIVY

WEITY (I) - weighting of the Ith division in the y-direction in block KBLOC

Group 10

WEITZ (I), I = 1, NDIVZ (only if NDIME = 3)

WEITZ (I) - weighting of the Ith division in the z-direction in block KBLOC

Group 11 (only if NDIME = 3)

XV, YV, ZV

XV - x-coordinate of viewing point for 3-D plot

YV - y-coordinate of viewing point for 3-D plot

ZV - z-coordinate of viewing point for 3-D plot

NOTE: XV = 300, YV = 300, ZV = 50 gives a good viewing angle for many problems.

Group 12 (only if NDIME = 3)

XMIN, XMAX, YMIN, YMAX, ZMIN, ZMAX

XMIN - minimum x-coordinate for plot of mesh

XMAX - maximum x-coordinate for plot of mesh

If XMIN = XMAX then the limits will be determined from the generated mesh

YMIN - minimum y-coordinate for plot of mesh

YMAX - maximum y-coordinate for plot of mesh

If YMIN = YMAX then the limits will be determined from the generated mesh

ZMIN - minimum z-coordinate for plot of mesh

ZMAX - maximum z-coordinate for plot of mesh

If ZMIN = ZMAX then the limits will be determined from the generated mesh

### Group 13 (optional)

NREF, XR, YR, ZR, IRFN

NREF - reference node for refinement

XR - x-coordinate of reference node

YR - y-coordinate of reference node

ZR - z-coordinate of reference node

IRFN - refinement level for reference node

If  $NREF < 0$  then the node closest to the reference coordinates is used as the reference node. If  $IRFN < 0$  then the node closest to the reference coordinates is used as the reference node and the coordinates set to the reference coordinates.

The refinement level is  $ABS(IRFN)$ . If the refinement level is 1 then the elements surrounding the reference node are subdivided once and new elements created. A refinement level of 2 means this is done twice, and so on.

Note on plotting. If  $KF \neq 0$  in Group 2 a plot of the mesh is provided, and if  $ABS(KF) > 1$  node numbers are printed on the plot.

### B. Macro Command Input For FEHMN

The finite element heat and mass transfer code (FEHMN) contains a macro control structure for data input that offers added flexibility to the input process. Blocks of data can be entered in any order, and any blocks unnecessary to a particular problem can be disregarded. All entries are free format, which adds flexibility, but requires that values be entered for all input variables (no assumed null values). As an aid to the user, the capabilities of FEHMN are summarized in Table IV with reference to the macro commands. Values of parameters are entered either by node number or a geometric description (macro command ZONE). The user is encouraged to read the macro ZONE description.

---



---

**TABLE IV. Capabilities of FEHMN with Macro Command References**

---

- I. Mass, energy balances in porous media
    - A. Variable rock properties (**ROCK**)
    - B. Variable permeability (**PERM**)
    - C. Variable thermal conductivity (**COND**)
    - D. Variable fracture properties, dual porosity (**DUAL**)
  
  - II. Multiple components available
    - A. Air water mixture available, fully coupled to heat and mass transfer (**NCON**)
    - B. Up to 10 passive tracers available (**TRAC**)
    - C. Several different capillary pressure models (**CAP**)
    - D. Several different relative permeability models (**RLP**)
  
  - III. Equation of state flexibility inherent in code (**EOS**)
  
  - IV. Psuedo-stress models available
    - A. Linear porosity deformation (**PPOR**)
    - B. Gangi stress model (**PPOR**)
  
  - V. Numerics
    - A. Finite element with multiple element capabilities (**ELEM**)
    - B. Short form input methods available (**COOR, ELEM**)
    - C. Flexible properties assignment (**ZONE**)
    - D. Flexible solution methods
      - 1. Upwinding, implicit solution available (**CTRL**)
      - 2. Iteration control adaptive strategy (**ITER**)
  
  - VI. Flexible time step and stability control (**TIME**)
- 
- 

**TABLE V. FEHMN Files**

---

TAPEn1( $1 \leq n1 \leq 10$ )	input file (user supplied)
TAPEn2( $11 \leq n2 \leq 20$ )	output file (code generated)
TAPEn3( $21 \leq n3 \leq 30$ )	initial value tape (read a restart, user supplied)
TAPEn4( $31 \leq n4 \leq 40$ )	final value tape (write a restart, code generated)
FE.HIS	time history of variables (code generated)
FE.CON	contour plot data (code generated)
FE.MIS	contains program information of the code crashes (code generated)
FE.TRC	tracer time history data (code generated)
STOR.FE	storage of finite element coefficients (user supplied or code generated)
FE.CHK	contains input analysis

---



---

Although most input data are contained in the input deck, some information must first be entered from the terminal. Most of the information required before the input deck can be read pertains to input and output files and is prompted for from within the program. Figure 7 shows the output for a typical FEHMN run on a CRAY computer. All files are of the form TAPEn, where *n* is the tape (unit) number. Table V contains a description of FEHMN files. The terminal input follows:

(free format) INPT, IOU, IREAD, ISAVE, IDC

INPT - unit number of the input file

IOU - unit number of the file to which nodal information (pressures, enthalpies, etc.) is printed

IREAD - unit number of file on which initial values of pressure and enthalpy are found. (If IREAD = 0, initial values are generated from input data. See macro control statement PRES)

ISAVE - unit number of file on which final time nodal information is printed for restart purposes (if ISAVE = 0, no restart file is created).

IDC - user subroutine parameter

if IDC = 0 the code makes no USER subroutine calls

if IDC  $\neq$  0 the code calls subroutine USER (user defined) at each time step.

The form is CALL USER (IDC).

In Fig. 8, the user entered data is after the "?". Here INPT = 1, IOU = 11, IREAD = 0, ISAVE = 0, and IDC = 0. The remainder of the data is read from unit INPT (which was defined above).

The macro command structure makes use of a set of control statements recognized by the input module of the program. When a macro control statement is encountered in the input deck, a certain set of data is expected and read from the input deck. In this way, the input is divided into separate, unordered blocks of data. The input deck is therefore a collection of macro control statements, each followed by its associated data block, as the example input files (Section D) show. Note that, although the input is free format, macro control statements must appear in the first four columns of a line. Table VI lists the macro control statements with brief descriptions of the data associated with each. The macro control statements may be in any order, although the data associated with each macro control statement must follow with the prescribed format. Some statements are necessary and others are optional, as indicated in Table VI.

A detailed list of the macro control statements and the input variables associated with each is given in Table VII. In Section D example input files are given.



```

xfehmz / 6 1.2
version fehm.4.0 ,george zyvoloski(505 6671581)

**** program files must obey the following conventions ****

        input files: tapel-10
        output files: tapell-20
        read files(if they exist): tape21-30
        write files(if they exist): tape31-40

**** note ****

        history plot file is fe.his
        contour plot file is fe.con
        tracer plot file is fe.trc
        input check file is fe.chk
        fe.mis is used for error recovery

**** and ****

        tape59(terminal) is available for any use

input tape,output file,rd tape,wt tape,user call/step
? 1 11 0 0 0
input title : node
input title : rlp
input title : sol
input title : init
input title : rock
input title : cond
input title : perm
input title : flow
input title : time
input title : ctrl
input title : coor
input title : elem
input title : stop
stop
xfehmz      ctss time      41.483      seconds
cpu=        18.305 i/o=      2.519 mem=      20.660

```

Fig. 7. Terminal output for a FEHMN run on a CRAY computer.

---



---

TABLE VI. Macro Control Statements for FEHMN

---

Control Statement	Description
CAP	capillary pressure data, optional.
COOR	node coordinate data, <b>required</b> .
COND	thermal conductivity data, <b>required</b> .
CONT	contour plot data, optional.
CTRL	program control parameters, <b>required</b> .
DUAL	input for dual porosity solution, optional.
ELEM	element node data, <b>required</b> .
EOS	equation of state data, optional.
FLOW	flow data, optional.
HFLX	heat flux data, optional.
INIT*	initial value data, optional.
ITER	iteration parameters, optional.
NGAS	noncondensable gas (air) data, optional.
NODE	node numbers for output and time histories, <b>required</b> .
PERM	permeability and velocity data, <b>required</b> .
PPOR	pressure and temperature dependent porosity and permeability, optional.
PRES	initial pressure and enthalpy data, optional.
RLP	relative permeability data, optional ( <b>required</b> for 2-phase problem).
ROCK	rock density, specific heat, and porosity data, <b>required</b> .
SOL	solution specifications, <b>required</b> .
STEADY	steady state solution generated for initial variable field, optional.
STOP	signals the end of input, <b>required</b> .
TEXT	text input, optional.
TIME	time step and time of simulation data, <b>required</b> .
TRAC	tracer data, optional.
ZONE	geometric definition of grid for input definition, optional.

---

\*One or both INIT and PRES macros are necessary.

---

The user is encouraged to look at the file FE.CHK. This file contains information on where the maximum and minimum input parameters occur and suggestions on decreasing the storage requirements for the run; it also summarizes initial mass and energy values.

Many input parameters such as porosity or permeability vary throughout the grid and need to be assigned different values on different nodes. This is accomplished in two ways. The first is a nodal loop-type definition:

JA,JB,JC,PROP1,PROP2, ...

where

- JA - first node to be assigned with the properties PROP1, PROP2 ...
- JB - last node to be assigned with the properties PROP1, PROP2 ...
- JC - loop increment for assigning properties PROP1, PROP2, ...
- Prop1, Prop2 - properties to be assigned to the nodes.

In the input blocks to follow one or more properties are manually entered in the above structure. When a value of 0 is entered for any JA, that input block is terminated and the code proceeds to the next group or control statement.

The nodal definition above is useful in simple geometries where the node numbers are easily found. The boundary nodes, in this case come at regular node intervals and the increment counter JC can be adjusted so the boundary conditions are easily entered.

In more complicated geometries, such as 3-D grids, the node numbers are often difficult to determine. Here a geometric description is preferred. To enable the geometric description the control statement ZONE (p. 74) is used in the input file before the other property macro statements occur. The input macro ZONE requires the specification of the coordinates of 4-node parallelograms for 2-D problems and the 8-node polyhedrons in 3-D. In one usage of the control statement ZONE all the nodes are placed in geometric zones and assigned an identifying number. This number is then addressed in the property input macro commands by specifying a  $JA < 0$  in the definition of the loop parameters given above. For example if  $JA = -1$ , the properties defined on the input line would be assigned to the nodes defined as belonging to geometric Group 1. The control statement ZONE may be called more than once to redefined geometric groupings.

---



---

TABLE VII. Input Description for FEHMN

---

**Control Statement CAP (optional)**

Capillary pressure model [see Eq. (29)]

Group 1- ICAP(i), cp1(i), cp2(i), cp3(i),

ICAP(i) - Relative permeability model type

ICAP(i) = 1, linear capillary pressure

cp1(i) - maximum capillary pressure

cp2(i) - maximum liquid saturation for capillary pressure calculation

cp3(i) - not used

Note: Only ICAP(I) = 1 is allowed. The parameter i is incremented each time a Group 1 line is read. Group 2 lines will refer to this parameter. Group 1 is ended when a line with ICAP(i) = 0 is encountered.

Group 2- JA, JB,JC, ICAPT

JA, JB, JC - defined on page 60

ICAPT - reference counter for model defined in Group 1

It is recommended that macro CAP be preceded by macro RLP because capillary pressures are defined in macro RLP if van Genuchten models are employed. Care should be taken to ensure that capillary pressures are not defined twice.

**Control statement COOR (required)**

Group 1 - N

N - number of nodes in the grid

Group 2 - MB, CORD1, CORD2, CORD3

MB - node number. If MB < 0 then the difference between the absolute value of MB and the previously read absolute value of MB is used to generate intermediate values by interpolation.

CORD1 - x-coordinate (m) of node MB

CORD2 - y-coordinate (m) of node MB

CORD3 - z-coordinate (m) of node MB

NOTE: To end the control section a line with MB = 0 is entered.

**Control statement COND (required)**

Assign thermal conductivities of the rock [see Section I-B, Eq. (6)]

Group 1 - JA, JB, JC, THXD, THYD, THZD

JA, JB, JC - defined on page 60

THXD - thermal conductivity (W/mK) in the x-direction

THYD - thermal conductivity (W/mK) in the y-direction

THZD - thermal conductivity (W/mK) in the z-direction

**Control statement CONT (optional)**

Group 1 - NCNTR, CONTIM

NCNTR - time step interval for contour plots

CONTIM - time (days) interval for contour plots

NOTE: the contour data will be output whenever either of the above criteria is satisfied

**Control statement CTRL (required)**

Assign various control parameters needed for equation solvers and matrix solver routines (see Section I-D)

Group 1 - MAXIT, EPM, NORTH [see Eqs. (55)-(68)]

- MAXIT - maximum number of iterations allowed in either the overall Newton cycle or the inner cycle to solve for the corrections at each iteration [see Eqs. (55)-(57) and Eqs. (63)-(68)]
- EPM - tolerance for Newton cycle (nonlinear equation tolerance)
- NORTH - number of orthogonalizations in the linear equation solver [see Eqs. (63)-(65)]

Group 2 - JA, JB, JC, IGAUS [see Eqs. (58)-(62)]

- JA, JB, JC - defined on page 60
- IGAUS - the order of partial Gauss elimination

Group 3 - AS, GRAV, UPWGT

- AS - implicitness factor [see Eq. (40)]  
if  $AS \leq 1$ , a standard pure implicit formulation will be used  
if  $AS \geq 1$ , a second-order implicit method will be used
- GRAV - direction of gravity 1 = x-direction, 2 = y-direction, 3 = z-direction. If  $GRAV > 3$ , GRAV is set equal to 3. If  $GRAV = 0$ , then no gravity is used. If  $GRAV \neq 0$  then a value of gravity of  $9.8 \text{ m/s}^2$  is used in the code.
- UPWGT - value of upstream weighting ( $0.5 \leq UPWGT \leq 1.0$ ) [see Sec. I-C, and the paragraph following Eq. (49)]  
If  $UPWGT < 0.5$  UPWGT is set to 0.5  
If  $UPWGT > 1.0$  UPWGT is set to 1.0

Group 4 - IAMM, AIAA, DAYMIN, DAYMAX

- IAMM - maximum number of iterations for which the code will multiply the time step size
- AIAA - time step multiplier (see Sec. I-D)
- DAYMIN - minimum time step size (days)
- DAYMAX - maximum time step size (days)

Group 5 - ICNL, LDA

- ICNL - parameter that specifies the geometry
  - if  $ICNL = 0$  three-dimensional
  - if  $ICNL = 1$  X - Y slice
  - if  $ICNL = 2$  X - Z slice
  - if  $ICNL = 3$  Y - Z slice

if ICNL = 4        X - Y radial slice  
 if ICNL = 5        X - Z radial slice  
 if ICNL = 6        Y - Z radial slice

**LDA** - parameter that specifies the external storage of  
 geometric coefficients  
**LDA = +1**, element coefficients are read in from file **STOR.FE**  
 and no coefficients are calculated in the code (note: **STOR.FE**  
 must be in local file space)  
**LDA = 0**, element coefficients are calculated in the code  
 and not saved  
**LDA = -1**, element coefficients are calculated in the code and  
 saved on file **STOR.FE**

**Control statement DUAL** (optional, see Section F)

**Group 1** - **JA, JB, JC, VOLFD1**  
**JA, JB, JC** - defined on page 60  
**VOLFD1** - volume fraction for first matrix node

**Group 2** - **JA, JB, JC, VOLFD2**  
**JA, JB, JC** - defined on page 60  
**VOLFD2** - volume fraction for second matrix node

**Group 3** - **JA, JB, JC, APUVD**  
**JA, JB, JC** - defined on page 60  
**APUVD** - area per unit volume (length scale) for the matrix nodes

The quantities **VOLFD1** and **VOLFD2** are volume fractions and related to the total volume  
 by

$$\text{VOLFD1} + \text{VOLFD2} + \text{VOLFF} = 1.0$$

where **VOLFF** is the volume fraction of the fractures. The above relation must be satisfied  
 at all nodes.

**Control statement ELEM** (required)

**Group 1** - **NS, NEI**,  
**NS** - number of nodes per element  
**NEI** - number of elements

**Group 2** - **MB, NELM (1), NELM (2)... NELM (NS)**  
**MB** - node number. If **MB < 0** then the difference between the

absolute value of MB and the previous absolute value of MB is used to generate intermediate values by interpolation in the code.

- NELM (1) - first node of element MB
- NELM (2) - second node of element MB
- NELM (NS) - last node of element MB

NOTE: To end the control section a line with MB = 0 is entered.

### Control Statement EOS (optional)

Equation of state, see pages 8-9)

#### Group 1 - IIEOSD, IPSAT, ITSAT

- IIEOSD - equation of state reference number. IIEOSD = 1 or 2 refer to high and low pressure data sets respectively in FEHMN. For these values the input in Group 2 and Group 3 will be ignored after it is entered.
- IPSAT - parameter to set vapor pressure to zero. If IPSAT  $\neq$  0 the vapor pressure is set to zero, otherwise the vapor pressure is calculated in the code.
- ITSAT - parameter to adjust the saturation temperature. If ITSAT < 0, the saturation temperature is set to -1000°C. If ITSAT > 0, the saturation temperature is set to 1000°C.

#### Group 2 - EW1, EW2, EW3, EW4, EW5, EW6,

EW7, EW8, EW9, EW10, EW11

- EW1 - liquid reference pressure
- EW2 - liquid reference temperature
- EW3 - liquid reference density
- EW4 - derivative of liquid density with respect to pressure at reference conditions
- EW5 - derivative of liquid density with respect to temperature at reference conditions
- EW6 - liquid reference enthalpy
- EW7 - derivative of liquid enthalpy with respect to pressure at reference conditions
- EW8 - derivative of liquid enthalpy with respect to temperature at reference conditions
- EW9 - liquid reference viscosity
- EW10 - derivative of liquid viscosity with respect to pressure at reference conditions

EW11 - derivative of liquid viscosity with respect to temperature  
at reference conditions

Group 3 - EV1, EV2, EV3, EV4, EV5, EV6,  
EV7, EV8, EV9, EV10, EV11

EV1 - vapor reference pressure

EV2 - vapor reference temperature

EV3 - vapor reference density

EV4 - derivative of vapor density with respect to pressure at  
reference conditions

EV5 - derivative of vapor density with respect to temperature at  
reference conditions

EV6 - vapor reference enthalpy

EV7 - derivative of vapor enthalpy with respect to pressure at  
reference conditions

EV8 - derivative of vapor enthalpy with respect to temperature at  
reference conditions

EV9 - vapor reference viscosity

EV10 - derivative of vapor viscosity with respect to pressure at  
reference conditions

EV11 - derivative of vapor viscosity with respect to temperature at  
reference conditions

### Control statement FLOW (optional)

[see Eq. (54)]

Group 1 - JA, JB, JC, SKD, EFLOW, AIPED

JA, JB, JC - defined on page 60

SKD - heat and mass source strength (kg/s), heat only (MJ/s).  
Negative value indicates injection into the rock mass.

EFLOW - enthalpy (MJ/kg) of fluid injected. If the fluid is flowing from  
the reservoir, then the in-place enthalpy is used. If  $EFLOW < 0$ ,  
then  $ABS(EFLOW)$  is interpreted as a temperature and the enthalpy  
calculated accordingly. In heat only problems with  $EFLOW < 0$ ,  
the node is in contact with a large heat pipe that supplies heat  
to the node through an impedance AIPED so as to maintain its  
temperature near  $ABS(EFLOW)$ . Large values (approximately  
1000) of AIPED are recommended.

AIPED - impedance parameter. If AIPED is nonzero, the code interprets  
SKD as a flowing wellbore pressure (MPa) with an impedance



ABS(AIPED). If AIPED < 0, flow is only allowed out of the well. For heat only, AIPED is the thermal resistance. If AIPED = 0, SKD is flow rate.

NOTE: If the porosity of the node is zero, then there is only a temperature solution, and the code forms a source proportional to the enthalpy difference E-EFLOW, where E is the in-place enthalpy and EFLOW is a specified enthalpy. The source term is given by  $Q = \text{AIPED} (E - \text{EFLOW})$ .

**Control Statement HFLX (optional)**

Group 1 - JA, JB, JC, FLUX, QFLXM

JA, JB, JC - defined on page 60

QFLUX - If QFLXM = 0, then AFLUX is the heat flux (MW) if QFLXM  $\neq$  0, then QFLUX is a temperature and the heat flux is calculated according to the formula:  $Q_H = QFLXM(TL - QFLUX)$

QFLXM - multiplier for heat flux equation given in QFLUX description (MW/°C)

**Control Statement INIT (optional)**

Set initial pressure and temperature at all nodes

Group 1 - PEIN, TIN, TIN1, GRAD1, DEPTH, TIN2, GRAD2, QUAD

PEIN - initial value of pressure (MPa). If initial values are read from IREAD (see terminal input), then this value is ignored. If gravity is present, this is the value of the pressure at node 1, and the other nodal pressures are adjusted by considering the hydraulic head.

TIN - initial value of temperature (°C). If TIN  $\leq$  0, then the initial temperatures are calculated using the pressure and temperature gradient.

NOTE: The initial temperatures are set according to the following formulas only if TIN  $\leq$  0. Otherwise, the initial temperatures are determined from PEIN and TIN.

$$0 \leq Z \leq \text{DEPTH} \quad T = \text{TIN1} + \text{GRAD1} \times Z$$

$$Z > \text{DEPTH} \quad T = \text{TIN2} + \text{GRAD2} \times Z + \text{QUAD} \times Z^2$$

TIN1 - defined in formulas above (°C)

GRAD1 - defined in formulas above (°C/m)

DEPTH - defined in formulas above (m)

TIN2 - defined in formulas above (°C)

GRAD2 - defined in formulas above (°C/m)

QUAD - defined in formulas above ( $^{\circ}\text{C}/\text{m}^2$ )

Control statement ITER (optional, see defaults below)

NOTE: If the user is not familiar with the linear equation solver routines in FEHMN please leave out control statement ITER and associated lines (see Section I-D).

Group 1 - G1, G2, G3, TMCH, OVER

- G1 - multiplier for the linear convergence region of the Newton-Raphson iteration
- G2 - multiplier for the quadratic convergence region of the Newton-Raphson iteration
- G3 - tolerance for the adaptive implicit method (multiplying factor for Newton-Raphson tolerance)
- TMCH - machine tolerance. If satisfied by the residual norm, the Newton iteration is complete
- OVERF - over relaxation factor for passive nodes in adaptive implicit method

Group 2 - IRDOF, ISLORD, IBACK, ICOUPL, RNMAX

- IRDOF - enables the reduced degree of freedom method
- ISLORD - reordering parameter. The ordering can be understood by labeling the mass equation as 1, the heat equation as 2, and the  $\text{CO}_2$  equation (if it exists) as 3. The value of ISLORD and the corresponding equation order is given below.

ISLORD	Mass, Heat	Mass, Heat, $\text{CO}_2$
0	1, 2	1, 2, 3
1	2, 1	1, 3, 2
2		2, 1, 3
3		2, 3, 1
4		3, 1, 2
5		3, 2, 1

the ordering has an effect on the speed of convergence of several solution algorithms, but will not affect most users

- IBACK - back substitution parameter
- ICOUPL - number of SOR iteration used in reduced degree of freedom methods
- RNMAX - maximum running time for problem before the solution is stopped

If control statement ITER is not present the following default values are used  $G1 = 0.001$ ,

$G2 = 0.0001$ ,  $G3 = 0.0001$ ,  $TMCH = 10^{-8}$ ,  $OVERF = 0.0$ ,  $IRDOF = 0$ .

**Control statement NGAS (optional)**

Noncondensable gas transport

Group 1 - ICO2D

ICO2D - solution descriptor for noncondensable gas transport

ICO2D - 0 data from control group NGAS is read but not used

ICO2D - 1, 2, reduced degree of freedom solver technology is used

ICO2D - 3, full 3 degrees of freedom solution water/noncondensable gas solution

Group 2 - JA, JB, JC, PCO2

JA, JB, JC - defined as in control statement ROCK

PCO2 - initial partial pressure of non-condensable gas. If  $PCO2 < 0$  then ABS (PCO2) is interpreted as a temperature and the partial pressure of the noncondensable gas is calculated according to the formula:  $PCO2 = P_T - P_{SAT}(T)$  where  $P_T$  is the total pressure and  $P_{SAT}(T)$  is the water saturation pressure and is a function of temperature only.

Group 3 - JA,  
JB,  
JC,  
CPNK

JA, JB, JC - defined on page 60

CPNK - injection concentration of noncondensable gas for injection mode ( $SK(i) < 0$ ). If it is a production node ( $SK(i) > 0$ ) then the in place concentration is used.

Note: For compatibility with older versions the user may substitute "CO2I" for "NGAS" in the input file.

**Control statement NODE (required)**

Specify the node numbers for which detailed printed output is desired. The plotting post-processor FEHPLTR will also use these nodes.

Group 1 - M

M - number of nodes for which information will be printed on IOUT (see terminal input). If  $M < 0$ , pressure and temperature will be written for all nodes.

Group 2 - MN (1), MN (2) ... MN (M)

MN - node numbers for which information will be printed on IOUT,  
M nodes (see Group 1).

If  $NN(I) < 0$ , then coordinates are used to define the print-out  
node. The coordinate sets (x, y, z) for each  $NM(I) < 0$  are added  
after Group 2. For 2-D problems put  $z = 0$ .

**Control statement PERM** (required)

Assign absolute permeabilities of the rock [see section I-B, Eq. (7)-(8)]

Group 1 - JA, JB, JC, PNXD, PNYD, PNZD

JA, JB, JC - defined on page 60

PNXD - permeability in the x-direction ( $m^2$ )

PNYD - permeability in the y-direction ( $m^2$ )

PNZD - permeability in the z-direction ( $m^2$ )

**Control Statement PPOR** (Optional, default is IPOROS=0)

For variable porosity/permeability problems, define model type (see Section I-B)

Group 1 - IPOROS, R1, R2, R3

IPOROS - Porosity/permeability type [see Eqs. (39)-(42)]  
= 0 constant porosity  
= 1 simple linear model  
= 2 Gangi stress model

R1,R2,R3 - parameters used in the various models

Group 2 - JA, JB, JC, R4, R5

JA,JB,JC - defined on page 60

R4 - variable parameter used in porosity/permeability models

R5 - variable parameter used in porosity/permeability models

Parameter	Model	
	Linear (Eq. 39)	Gangi(Eq. 40-41)
R1	$C_r$	$\alpha$
R2	$C_g$	E
R3	not used	$\sigma$
R4	not used	m(exponent)
R5	not used	$P_o$

For the linear model  $P_o$  is PEIN in macro INIT.  $\phi_o$  is PSD in macro ROCK and  $k_o$  is from macro PERM for both models.

**Control statement PRES (optional)**

Assign nonuniform initial pressure and temperature values

Group 1 - JA, JB, JC, PHRD, TIND, IEOSD

- JA, JB, JC - defined on page 60
- PHRD - initial pressure (MPa)
- TIND - initial temperature (If IEOSD = 1 or 3) or initial saturation (if IEOSD = 2)
- IEOSD - thermodynamic region parameter if IEOSD = 1, then in compressed liquid region, if IEOSD = 2, the saturation region, if IEOSD = 3, the superheated region.

NOTE: The initial values defined in control statement PRES supersede all others.

**Control statement RLP (optional)**

Relative permeability models [see Eqs. (25)-(27)]

Group 1 - IRLP(i), RP1, RP2, RP3, RP4

IRLP - Relative permeability model type

IRLP(i) = 1 linear type

RP1 - irreducible liquid saturation

RP2 - irreducible vapor saturation

RP3 - maximum liquid saturation

RP4 - maximum vapor saturation

IRLP(i) = 2 Corey type

RP1 - irreducible liquid saturation

RP2 - irreducible vapor saturation

RP3 - not used

RP4 - not used

IRLP(i) = 3 van Genuchten (note different input)

NOTE: With a van Genuchten formulation (IRLP=3, IRLP=4), both the relative permeability and capillary information are input. Therefore there is no capillary pressure input and information should not be input in the capillary pressure section (macro CAP) for those nodes.

RP1, RP2, RP3, RP4, RP5, RP6

RP1 - residual liquid saturation

RP2 - maximum liquid saturation

RP3 -  $\alpha$ , parameter for model

RP4 -  $\beta$  parameter for model

RP5 - maximum capillary pressure

RP6 - fractional difference in pressure at maximum and cutoff saturation  
 IRLP(i) = 4 combined van Genuchten model. All the values for IRLP = 3 are  
 read in plus the following RP7, RP8, RP9, RP10, RP11, RP12, RP13,  
 RP14, RP15  
 RP7 - residual liquid saturation for fracture  
 RP8 - maximum liquid saturation for fracture  
 RP9 -  $\alpha$ , for fractures  
 RP10 -  $\beta$ , for fractures  
 RP11 - maximum capillary pressure for fracture  
 RP12 - fractional difference in pressure at maximum and cutoff saturation  
 RP13 - fracture intrinsic permeability ( $m^2$ )  
 RP14 - matrix intrinsic permeability ( $m^2$ )  
 RP15 - fracture porosity

Group 1 is ended when a line with IRLP(i) = 0 is encountered.

Group 2 - JA, JB, JC, I

JA, JB, JC - defined on page 60

I - number referring to the sequence of models read in Group1

NOTE: The parameter  $i$  is incremented each time a Group 1 line is read. Group 2 lines will refer to this parameter.

**Control statement ROCK (required)**

Assign rock density, specific heat and porosity [see Section I-B, Eqs. (1)-(10)]

Group 1 - JA, JB, JC, DENRD, CPRD, PSD

JA,JB,JC - defined on page 60

DENRD - rock density ( $kg/m^3$ )

CPRD - rock specific heat ( $MJ/kg/^\circ C$ ). If CPRD > 1 the code will  
 assume the units are  $J/kg/^\circ C$  and multiply by  $10^{-6}$

PSD - porosity

**Control Statement SOL (required)**

Group 1 - NTT, INTG

NTT - parameter that defines the type of solution required

if  $NTT \geq 0$  heat and mass transfer solution

if  $NTT < 0$  heat transfer solution

INTG - parameter that defines element integration type

(refer to Section I-B)

if  $INTG \leq 0$  Lobatto quadrature is used, recommended for  
 heat and mass problems without stress.

if  $INTG > 0$  Gauss quadrature is used, recommended for problems requiring a stress solution.

### **Control Statement STEA**

No input is associated with this macro statement. This statement enables a 1-D solution in the y-direction (2-D) or z-direction (3-D) when gravity is present to generate an initial steady state solution.

### **Control Statement STOP (required)**

NOTE: No input is associated with this control statement. It signals the end of input, and as such it always appears as the last line of an input deck.

### **Control Statement TEXT**

Following the control statement, text is input until a blank line is inserted to signal the end of the control statement. This text is printed on the output file.

### **Control statement TIME (required)**

Group 1 - DAY, TIMS, NSTEP, II, YEAR, MONTH

- DAY - initial time step size (days)
- TIMS - simulation maximum time (days)
- NSTEP - maximum number of time steps allowed
- II - print-out interval for nodal information (pressure, enthalpy etc.), as set up under control statement node.
- YEAR - year that simulation starts
- MONTH - month that simulation starts

Group 2 - DIT1, DIT2, DIT3, ITC

- DIT1 - time (days) for time step change
- DIT2 - new time step size (days). If  $DIT2 < 0$  then  $ABS(DIT2)$  is the new time step multiplier
- DIT3 - implicitness factor for new time step (use  $\leq 1.0$  backward Euler,  $> 1.0$  for second-order implicit scheme).
- ITC - new print-out interval

NOTE: The code proceeds to the next control statement when a line is encountered with  $DIT1 = 0$ . A contour plot will be drawn at each DIT1. A restart file will be written at each DIT1.

**Control statement TRAC (optional)**

[see Eqs. (16)-(19) and (22)-(24) and Table II]

**Group 1 - ANO, AWC, EPC, UPWGTA**

- ANO - initial tracer concentration
- AWC - Implicitness factor for tracers.  $AWC > 1.0$  gives 2nd order solution;  $AWC \leq 1.0$  gives 1st order solution
- EPC - equation tolerance for tracer solution
- UPWGTA - upstream weighting term for the tracer solution  
If  $UPWGTA < 0.5$  UPWGTA is set to 0.5  
If  $UPWGTA > 1.0$  UPWGTA is set to 1.0

**Group 2 - DAYCS, DAYCF, DAYHF, DAYHS**

- DAYCS - time which the tracer solution is enabled
- DAYCF - time which the tracer solution is disabled
- DAYHF - time which the heat and mass transfer solution is disabled
- DAYHS - time which the heat and mass transfer solution is enabled

**Group 3 - IACCMX, DAYCM, DAYCMM, DAYCMX**

- IACCMS - maximum number of iterations allowed in tracer solution if time step multiplier is enabled
- DAYCM - time step multiplier for tracer solution
- DAYCMM - minimum time step for tracer solution
- DAYCMX - maximum time step for tracer solution

**Group 4 - NSPECIES**

- NSPECIES - number of different tracers

NOTE: TRAC groups 5, 6, 7, and 8 are entered as a unit for each different tracer.

**Group 5 - ICNS, IADSF, AIADSF, A2ADSF, BETAD**

- ICNS - phase designation. If  $ICNS \leq 0$  a gas phase tracer is used. If  $ICNS > 0$ , then a liquid phase tracer is used.
- IADSF - designates tracer type [see Eq. (23)-(24) and Table II]
  - = 0, refers to the conservative tracer
  - = 1, refers to the linear model
  - = 2, refers to the Freundlich model
  - = 3, refers to the modified Freundlich model
  - = 4, refers to the Langmuir model
- A1ADSF -  $\alpha_1$  parameter
- A2ADSF -  $\alpha_2$  parameter
- BETAD -  $\beta$  parameter



**Group 6 - ICRATE, A1R, A2R, A3R, A4R**

- ICRATE - designates reaction model type see Eq. (24).
- A1R - parameter in rate model
- A2R - parameter in rate model
- A3R - parameter in rate model
- A4R - parameter in rate model

ICRATE = 1 refers to the simple model (p. 9) and ICRATE  $\geq$  2 refers to the more complicated model (p. 9).

**Group 7 - JA, JB, JC, TCXD, TCYD, TCZD**

- JA,JB,JC - defined on page 60
- TCXD - dispersivity coefficient in the x-direction ( $m^2/s$ )
- TCYD - dispersivity coefficient in the y-direction ( $m^2/s$ )
- TCZD - dispersivity coefficient in the z-direction ( $m^2/s$ )

**Group 8 - JA, JB, JC, ANQO**

- JA,JB,JC - defined on page 60
- ANQO - initial concentration of tracer, which will supersede the value given by ANO in Group 1. Note that if initial values of pressure and enthalpy are read from a file, then the code will also read initial values for the tracer from the file.

**Group 9 - JA, JB, JC, CNSK, T1SK, T2SK**

- JA,JB,JC - defined on page 60
- CNSK - injection concentration of injection node. If it is a production node, then the in-place concentration is used
- T1SK - time (days) when tracer injection begins
- T2SK - time (days) when tracer injection ends

**NOTE:** Injection nodes must be specified in control statement flow.

**Control statement ZONE (Optional, default is input by nodes)**

**Group 1- IZONE**

- IZONE - identification number for geometric input

**Group 2- X1, X2, X3, X4, Y1, Y2, Y3, Y4 (for 2-D problems)**

- X1-X4 - X coordinates for zone IZONE
- Y1-X4 - Y coordinates for zone IZONE
- X1-X8, Y1-Y8, Z1-Z8 (for 3-D problems)
- X1-X8 - X coordinates for zone IZONE
- Y1-Y8 - Y coordinates for zone IZONE
- Z1-Z8 - Z coordinates for zone IZONE

NOTE: If the first four characters in Group 2 are 'LIST' then the code reads a list of x, y, z-coordinates, one set perline until a blank line is encountered. The nodes corresponding to these coordinates make up the zone. The geometric zone description is implemented by defining geometric regions. The coordinates given in Group 2 are defined in Fig. 5. All properties defined by node (JA, JB, JC) may be defined by ZONE. In the previous macro descriptions if  $JA < 0$ , then the zone  $IZONE = ABS(JA)$  is referenced. The macro ZONE must precede the usage of a ZONE reference. ZONE can be called more than once.

---

### C. Graphics Postprocessing

Two graphics postprocessing codes are described in this section. They are written using the DISSPLA graphics package. Except for the plot area specification only the primitive line drawing commands are used. Therefore the routines should be easily convertible to other systems. A capability for time history plots for variables (FEHPLTR) and contour plotting (FECPLTR) are provided. Though these codes have not been verified, users may use them at their convenience.

1. FEHPLTR is a postprocessor program for FEHMN. It uses output information from FEHMN in the file FE.HIS. The program organizes information found in the file FE.HIS for plotting time histories of the variables temperature, pressure, enthalpy, flow rate, concentration, and capillary pressure. The user input is found in file HIS.INS.

Group 1 - HEADER - 80 character title

Group 2 - NNODE - number of input nodes. This must correspond to the number of print-out nodes specified in the input file for FEHMN.

Group 3 - ITYPE, IPLOT (I), II=1, NNODE

ITYPE - variable designator  
= 1, enthalpy plot  
= 2, flow rate plot  
= 3, temperature plot  
= 4, pressure plot  
= 5, capillary pressure plot  
= 6, concentration plot

IPLOT(I) - designates if the Ith node is to be plotted on the current plot.  
IPLOT(I)  $\neq 0$  then the Ith node will be plotted.  
IPLOT(I) = 0 then the Ith node will not be plotted.

- Group 4- A - parameter to scale the plot variable according to the formula  
 $P^* = A(P-B)$   
 B - parameter to scale the plot variable according to the formula  
 given in the last description  
 C - parameter to scale the time variable according to the formula  
 $t^* = C(T - D)$   
 D - parameter to scale the time variable according to the formula  
 given in this last description

Note: If 0,0,0,0 is entered, no action is taken (i.e., P = p)

Group 5 - XLEN, YLEN

- XLEN - physical plot horizontal dimension in inches  
 YLEN - physical plot vertical dimension in inches

Group 6 - AXIS

- AXIS - plot type  
 AXIS < 0 time axis is a log axis and the variable axis is linear  
 AXIS = 0, both axes are linear  
 AXIS > 0, both axes are log scales

Group 7 - DAYMIN, DAYMAX, DAYTIC, NTIC

- DAYMIN - minimum limit for time axis  
 DAYMAX - maximum limit for time axis  
 DAYTIC - increment for time axis  
 NTIC - tic marks per increment for the time axis

Group 8 - VMIN, VMAX, VTIC, NIY

- VMIN - minimum limit for variable axis  
 VMAX - maximum limit for variable axis  
 VTIC - increment value for variable axis  
 NIY - tic marks per interval for the variable axis

Group 9 - TITLE

- TITLE - 30 character (max) heading for top of plot

Group 10 - TITLX

- TITLX - 30 character (max) heading for time axis

Group 11 - TITLY

TITLY - 30 character (max) heading for the variable axis

Group 12 is entered only if ITYPE = 6 is chosen and a concentration plot is generated. Since several (up to 10) concentration profiles can be plotted, the species number to be plotted must be specified. Group 12 provides this information.

Group 12 - [ISPT (II) II=1, NSPECI]

ISPT(II) - plot designator for the IIth specie

≠ 0 then that specie is plotted

= 0 then that specie is not plotted

NOTE: the variable NSPECI is obtained by the code from the file FE.HIS. Groups 3-12 may be repeated for additional plots.

2. **FECPLTR.** The computer code **FECPLTR** is the postprocessor code for **FEHMN** which makes contour plots. Its input file is the unformatted file **FE.CON** generated by **FEHMN**. The plot instruction commands are given in the file **CON.INS**. The input lines are described below and are in free format except where noted.

Group 1 - ICHOS

ICHOS - dimensionality parameter

= 2, 2 dimensional contour plots are generated

≠ 2, 3-dimensional contour plot information is provided

NOTE: the form of the input that follows is not implemented as yet for the value of ICHOS = 3.

Group 2 - HEADER

Header - title (80 characters maximum)

Group 3 - NCI, IGRID

NCI - contour label interval NCI = 0, no labels are drawn on contours, contours are given different line types (dash, solid, etc.) and identified on the side of the plot NCI ≠ 0, the contours are labeled on the contour line

IGRID - grid parameter

= 0, no grid drawn with contours

≠ 0, grid is drawn with contours

Group 4- AX, BX, AY, BY

AX - minimum x coordinate for problem (m)

BX - maximum x coordinate for problem (m)

- AY - minimum y coordinate for problem (m)
- BY - maximum y coordinate for problem (m)

Group 5- VLENM, VRMAX

- VLENM - length of maximum vector (in grid dimensions)
- VRMAX - size of maximum vector (m/s)

Group 6- XWIN, YWIN

- XWIN - physical size of the x direction of plot window (in)
- YWIN - physical size of the y direction of plot window (in)

Group 7- IVLP, CNTRT, CNTRP, CNTRC, SCALE

- IVLP - plot phase parameter IVLP < 0, vapor phase only plots will be drawn. IVLP > 0, liquid phase only plots will be drawn
- CNTRT - contour interval for temperature (liquid region) or saturation (vapor region)
- CNTRP - phase pressure contour interval
- CNTRC - phase contour interval for species transport
- SCALE - scaling parameter for velocity vectors. No vectors will be plotted for vectors of magnitude less than VRMAX \* SCALE (see Group 5).

Note: If CNTRT, CNTRP, CNTRC are < 0, then the contour values are provided in a user supplied list. (Group 8 is used.) If they are > 0 then Group 8 is not used.

Group 8 - NV, (CVAL(I), I = 1, NV)

- NV - number of contour values
- CVAL(I) - contour value (can be temperature, saturation pressure, or concentration)

If multiple contour plots are desired, the user may provide additional data sets for each plot (i.e., Groups 1-7). Alternatively, the user may specify the same parameter set for each plot by not providing additional sets in the data file CON.INS. This way all the plot sets output by FEHMN and in FE.CON will be plotted.

#### D. Example Input Files And Output Files

This section contains three example problem runs with FEHMN. Input files and output files are provided. Other examples may be found in the FEHMN software verification report (Zyvoloski and Dash, 1991).

1. **Heat Conduction.** This 3-D problem demonstrates the code performance on a purely conductive problem. It is useful in showing the numerical accuracy of the finite elements and providing the user with an example of 3-D input. While we give only the 4 x 4 x 4 mesh input and output, accuracy results are presented for the 4 x 4 x 4, 8 x 8 x 8, and 12 x 12 x 12 meshes. Table VIII shows the parameters used in the computer runs. Figure 8 depicts the problem geometry (due to symmetry only a quarter of the cube is depicted). Basically the cube is initially at 200°C and a boundary condition of 100°C is applied on all sides. Table IX gives the coordinate positions for the various error sampling points as well as defining the runs. As can be seen from Table X even the crudest grid produced errors of less than 9%. Other grids produced much better results. For the 4 x 4 x 4 grid, the input to the preprocessor GENMSH is shown in Fig. 9. The plot produced by GENMSH is given in Fig. 10. The input file for FEHMN is provided in Fig. 11. It is worth noting here that the part of the file from the macro command **COOR** to the end was produced by GENMSH (file GEOM.DAT) and appended to the other macro commands with a text editor. Figure 12 gives the output for the 4 x 4 x 4 run. The user

---



---

TABLE VIII. Input Parameters for the 3-D Heat Conduction Problem

---



---

Parameter	Symbol	Value
Rock thermal diffusivity	$^*\kappa$	
Rock thermal conductivity	$\kappa_r$	2.7 W/m K
Rock density	$\rho_r$	2700 kg/m <sup>3</sup>
Rock specific heat	$C_r$	1000 J/kgK
Width	a	0.5 m
Length	b	0.5 m
Depth	c	0.5 m
Initial temperature	$T_0$	200°C
Surface temperature	$T_s$	100°C
for all $x, y, z = 0.5$ m		

---



---


$$^*\kappa = \frac{\kappa_r}{\rho_r C_r}$$


---



---

**TABLE IX. Sample Problems for 3-D Heat Conduction**

Problem	3-D Mesh Elements
1	4 x 4 x 4 brick
2	8 x 8 x 8 brick
3	12 x 12 x 12 brick
4	8 x 8 x 8 prism
5	8 x 8 x 8 mixed brick and prism
Comparison coordinate positions	$x = 0.000 \ y = 0.000 \ z = 0.000$ $x = 0.000 \ y = 0.125 \ z = 0.250$ $x = 0.125 \ y = 0.250 \ z = 0.375$ $x = 0.375 \ y = 0.375 \ z = 0.375$

**TABLE X. Comparison of Analytical and Model Results for 3-D Heat Conduction**

Coordinate position	Maximum Error (%)				
	1	2	3	4	5
$x = 0.000 \ y = 0.000 \ z = 0.000$	2.139	0.710	0.427	0.718	0.570
$x = 0.000 \ y = 0.125 \ z = 0.250$	1.784	0.572	0.339	0.560	0.572
$x = 0.125 \ y = 0.250 \ z = 0.375$	3.546	1.382	0.862	1.372	1.382
$x = 0.375 \ y = 0.375 \ z = 0.375$	8.517	3.544	2.301	3.379	3.544

instruction file for the postprocessor FEHPLTR is shown in Fig. 13. The plot produced by FEHPLTR is given in Fig. 14.

**2. Toronyi Two-Phase Example.** This problem is a model of a two-phase, highly permeable geothermal reservoir originally proposed by Toronyi and Farouq Ali (1977) and solved by a number of authors (Mercer and Faust 1975, Thomas and Pierson 1978). The model reservoir is shown in Fig. 15. The input for the problem is presented in Table XI. As with Thomas and Pierson, time steps of 10 days with an initial time step of 8.3 days were used. The final state corresponds to 19% of the original water mass removed. Figure 15 also shows the results obtained in this study using quadrilateral elements compared with the results obtained by Thomas and Pierson. Good agreement is evident. This is somewhat surprising considering the elements have a length/width ratio of 10. The input for the GENMSH preprocessor is shown in Fig. 16. The input file is given in Fig. 17. The part of the input file from the macro COOR was generated by GENMSH and inserted in the input file using a text editor. Output for the first computer run is shown in Fig. 18.

TABLE XI. Parameters for Toronyi Example

Parameter	Symbol	Value
Reservoir permeability	$k$	$9.869 \times 10^{-13} \text{ m}^2$
Reservoir porosity	$\phi$	0.05
Rock thermal conductivity	$\kappa_r$	$1.73 \text{ W/m} \cdot \text{K}$
Rock density	$\rho_r$	$2500 \text{ kg/m}^3$
Rock specific heat	$C_r$	$1000 \text{ J/kg} \cdot \text{K}$
Aquifer length	—	1828 m
Aquifer width	—	182.8 m
Initial water saturation	$s_{ij}^0$	0.2
Aquifer discharge	$q_m$	$0.05 \text{ kg/m} \cdot \text{s}$
Initial Pressure	$P_{ij}^0$	4.4816 MPa

**3. DOE Code Comparison Project, Problem 5, Case A.** This problem involves multiphase flow in a 2-D horizontal reservoir. The problem is characterized by a moving two-phase region, i.e., the fluid produced at the production well is replaced by cold water recharge over one of the outer boundaries. The problem parameters are given in Table XII and the geometry and boundary conditions are shown in Fig. 19. Of particular note is the variable initial temperature field and the prescribed pressure and temperature boundary. This problem shows that two-phase coding as well as the phase change algorithm are working properly, since numerical difficulties can occur as nodes go from two-phase fluid to compressed water.

There is no analytical solution for this problem, but six researchers produced results for the DOE code comparison project (Molloy, 1980). The reader is referred to this reference for a more detailed discussion of this problem and the code comparison. Results from



this problem are compared to those from the other codes, obtained from Molloy (1980) as a check on FEHMN. The results for the outlet temperature, shown in Fig. 20, are in excellent agreement with the other codes. The results for the outlet pressure, Fig. 21, and pressure at an observation well 125 m distant, Fig. 22 are also in good agreement with the other codes.

The input for the preprocessor GENMSH is given in Fig. 23. The input to FEHMN is given in Fig. 24. The printout for the computer is provided in Fig. 25. The part of the input file from the macro COOR was generated by GENMSH. A contour plot of temperature was also generated for this problem. The user generated input file CON.INS is shown in Fig. 26. The contour plot is given in Fig. 27.

---



---

TABLE XII. Input Parameters for the DOE Code Comparison Project, Problem 5, Case A

---

Parameter	Symbol	Value
Reservoir permeability	$k$	$2.5 \times 10^{-14} \text{ m}^2$
Reservoir porosity	$\phi$	0.35
Rock thermal conductivity	$\kappa_r$	1 W/m · K
Rock density	$\rho_r$	2500 kg/m <sup>3</sup>
Rock specific heat	$C_r$	1000 J/kg · °C
Reservoir length	$x$	300 m
Reservoir thickness	$y$	200 m
Liquid residual saturation	$s_{lr}$	0.3
Gas residual saturation	$s_{gr}$	0.1
Reservoir discharge	$q_m$	0.05 kg/m · s)
Initial Pressure	$P_o$	3.6 MPa

---

Production well coordinates:  $x = 62.5 \text{ m}, y = 62.5 \text{ m}$

Observation well coordinates:  $x = 162.5 \text{ m}, y = 137.5 \text{ m}$

Initial temperature distribution:

$$T(x, y, 0) = \begin{pmatrix} 240 \\ 240 - 160 \left[ \frac{r-100}{200} \right]^2 + 80 \left[ \frac{r-100}{200} \right]^4 \\ 160 \end{pmatrix} \text{ } ^\circ\text{C} \quad \begin{matrix} r \leq 100 \text{ m} \\ 100 < r < 300 \text{ m} \\ r \geq 300 \text{ m} \end{matrix}$$

where  $r = \sqrt{x^2 + y^2}$

---



---

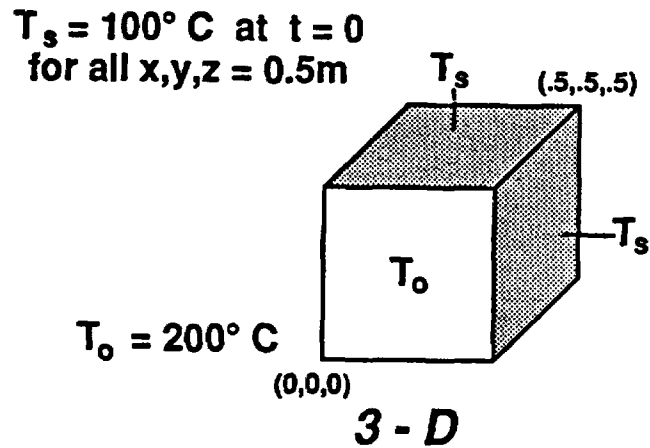


Fig. 8. Schematic diagram of the 3-D heat conduction problem.

```

1 3D Model of a Cube (4x4x4 cubes)
2 20 1 20 0 3 1 0
3 1 1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20
4 0.00 0.25 0.50 0.50 0.50 0.25 0.00 0.00
5 0.00 0.50 0.50 0.00
6 0.00 0.25 0.50 0.50 0.50 0.25 0.00 0.00
7 0.00 0.00 0.00 0.25 0.50 0.50 0.50 0.25
8 0.00 0.00 0.50 0.50
9 0.00 0.00 0.00 0.25 0.50 0.50 0.50 0.25
10 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00
11 0.25 0.25 0.25 0.25
12 0.50 0.50 0.50 0.50 0.50 0.50 0.50 0.50
13 1 4 4 4
14 1 1 1 1
15 1 1 1 1
16 1 1 1 1
17 300. 300. 50.0
18 0 0 0 0 0 0.

```

Fig. 9. Input for preprocessor GENMSH for 3-D heat conduction example.

3D Model of a Cube (4x4x4 cubes)

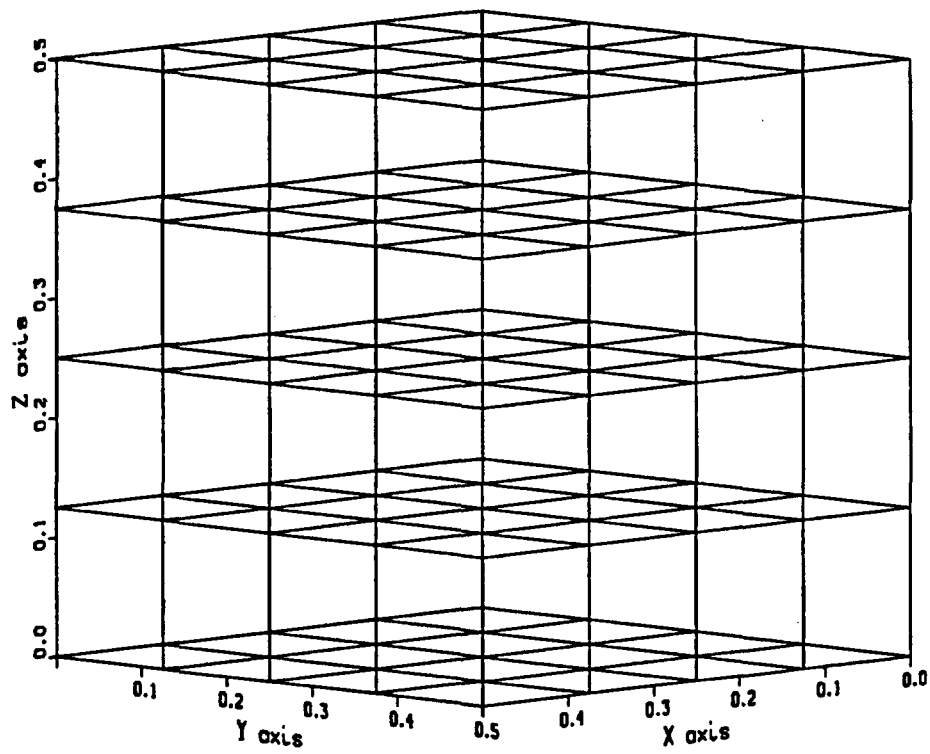


Fig. 10. Grid for 4 x 4 x 4 heat conduction problem.

```

***** 3-D Heat Conduction Model (4X4X4 cubes) *****
node
  8
  001 056 087 094
  005 025 002 125
rlp
2 0. 0. 0. 0.
0
1 125 1 1
0 0 0 0
sol
  -1  -1
init
  10.  0.  200.  0.  0.  200.  0.  0.
rock
  1 125 1 2700. 1000. 0. 1.0
  0 0 0 0. 0. 0. 0.
cond
  1 125 1 2.7e-00 2.7e-00 2.7e-00
  0 0 0 0. 0. 0.
perm
  1 125 1 1.e-30 1.e-30 1.e-30 0. 0. 0.
  0 0 0 0. 0. 0. 0. 0. 0.
flow
  101 125 1 10.00 -100.00 1.e03
  5 125 25 10.00 -100.00 1.e03
  10 125 25 10.00 -100.00 1.e03
  15 125 25 10.00 -100.00 1.e03
  20 125 25 10.00 -100.00 1.e03
  25 125 25 10.00 -100.00 1.e03
  21 125 25 10.00 -100.00 1.e03
  22 125 25 10.00 -100.00 1.e03
  23 125 25 10.00 -100.00 1.e03
  24 125 25 10.00 -100.00 1.e03
  0 0 0 0. 0. 0.
time
0.005 3.00 1000 1000 1989 04
0. 0. 0. 0
ctrl
  40 1.e-04 08
  1 125 1 1
  0 0 0 0
  1.0 0.0 1.0
  10 1.0 0.00005 0.005
  0 0
coor
  125
      1 0.00000 0.00000 0.00000
      2 0.12500 0.00000 0.00000
      3 0.25000 0.00000 0.00000
      4 0.37500 0.00000 0.00000
      5 0.50000 0.00000 0.00000
      6 0.00000 0.12500 0.00000
      7 0.12500 0.12500 0.00000
      8 0.25000 0.12500 0.00000
      9 0.37500 0.12500 0.00000
     10 0.50000 0.12500 0.00000
     11 0.00000 0.25000 0.00000
     12 0.12500 0.25000 0.00000
     13 0.25000 0.25000 0.00000

```

Fig. 11. Input file for FEHMN for 3-D heat conduction example.

14	0.37500	0.25000	0.00000
15	0.50000	0.25000	0.00000
16	0.00000	0.37500	0.00000
17	0.12500	0.37500	0.00000
18	0.25000	0.37500	0.00000
19	0.37500	0.37500	0.00000
20	0.50000	0.37500	0.00000
21	0.00000	0.50000	0.00000
22	0.12500	0.50000	0.00000
23	0.25000	0.50000	0.00000
24	0.37500	0.50000	0.00000
25	0.50000	0.50000	0.00000
26	0.00000	0.00000	0.12500
27	0.12500	0.00000	0.12500
28	0.25000	0.00000	0.12500
29	0.37500	0.00000	0.12500
30	0.50000	0.00000	0.12500
31	0.00000	0.12500	0.12500
32	0.12500	0.12500	0.12500
33	0.25000	0.12500	0.12500
34	0.37500	0.12500	0.12500
35	0.50000	0.12500	0.12500
36	0.00000	0.25000	0.12500
37	0.12500	0.25000	0.12500
38	0.25000	0.25000	0.12500
39	0.37500	0.25000	0.12500
40	0.50000	0.25000	0.12500
41	0.00000	0.37500	0.12500
42	0.12500	0.37500	0.12500
43	0.25000	0.37500	0.12500
44	0.37500	0.37500	0.12500
45	0.50000	0.37500	0.12500
46	0.00000	0.50000	0.12500
47	0.12500	0.50000	0.12500
48	0.25000	0.50000	0.12500
49	0.37500	0.50000	0.12500
50	0.50000	0.50000	0.12500
51	0.00000	0.00000	0.25000
52	0.12500	0.00000	0.25000
53	0.25000	0.00000	0.25000
54	0.37500	0.00000	0.25000
55	0.50000	0.00000	0.25000
56	0.00000	0.12500	0.25000
57	0.12500	0.12500	0.25000
58	0.25000	0.12500	0.25000
59	0.37500	0.12500	0.25000
60	0.50000	0.12500	0.25000
61	0.00000	0.25000	0.25000
62	0.12500	0.25000	0.25000
63	0.25000	0.25000	0.25000
64	0.37500	0.25000	0.25000
65	0.50000	0.25000	0.25000
66	0.00000	0.37500	0.25000
67	0.12500	0.37500	0.25000
68	0.25000	0.37500	0.25000
69	0.37500	0.37500	0.25000
70	0.50000	0.37500	0.25000
71	0.00000	0.50000	0.25000
72	0.12500	0.50000	0.25000
73	0.25000	0.50000	0.25000

Fig. 11. (Continued)

74	0.37500	0.50000	0.25000
75	0.50000	0.50000	0.25000
76	0.00000	0.00000	0.37500
77	0.12500	0.00000	0.37500
78	0.25000	0.00000	0.37500
79	0.37500	0.00000	0.37500
80	0.50000	0.00000	0.37500
81	0.00000	0.12500	0.37500
82	0.12500	0.12500	0.37500
83	0.25000	0.12500	0.37500
84	0.37500	0.12500	0.37500
85	0.50000	0.12500	0.37500
86	0.00000	0.25000	0.37500
87	0.12500	0.25000	0.37500
88	0.25000	0.25000	0.37500
89	0.37500	0.25000	0.37500
90	0.50000	0.25000	0.37500
91	0.00000	0.37500	0.37500
92	0.12500	0.37500	0.37500
93	0.25000	0.37500	0.37500
94	0.37500	0.37500	0.37500
95	0.50000	0.37500	0.37500
96	0.00000	0.50000	0.37500
97	0.12500	0.50000	0.37500
98	0.25000	0.50000	0.37500
99	0.37500	0.50000	0.37500
100	0.50000	0.50000	0.37500
101	0.00000	0.00000	0.50000
102	0.12500	0.00000	0.50000
103	0.25000	0.00000	0.50000
104	0.37500	0.00000	0.50000
105	0.50000	0.00000	0.50000
106	0.00000	0.12500	0.50000
107	0.12500	0.12500	0.50000
108	0.25000	0.12500	0.50000
109	0.37500	0.12500	0.50000
110	0.50000	0.12500	0.50000
111	0.00000	0.25000	0.50000
112	0.12500	0.25000	0.50000
113	0.25000	0.25000	0.50000
114	0.37500	0.25000	0.50000
115	0.50000	0.25000	0.50000
116	0.00000	0.37500	0.50000
117	0.12500	0.37500	0.50000
118	0.25000	0.37500	0.50000
119	0.37500	0.37500	0.50000
120	0.50000	0.37500	0.50000
121	0.00000	0.50000	0.50000
122	0.12500	0.50000	0.50000
123	0.25000	0.50000	0.50000
124	0.37500	0.50000	0.50000
125	0.50000	0.50000	0.50000
0	0.00000	0.00000	0.00000

elem	8,	64,	0						
1	1	2	7	6	26	27	32	31	
2	2	3	8	7	27	28	33	32	
3	3	4	9	8	28	29	34	33	
4	4	5	10	9	29	30	35	34	
5	6	7	12	11	31	32	37	36	

Fig. 11. Continued

6	7	8	13	12	32	33	38	37
7	8	9	14	13	33	34	39	38
8	9	10	15	14	34	35	40	39
9	11	12	17	16	36	37	42	41
10	12	13	18	17	37	38	43	42
11	13	14	19	18	38	39	44	43
12	14	15	20	19	39	40	45	44
13	16	17	22	21	41	42	47	46
14	17	18	23	22	42	43	48	47
15	18	19	24	23	43	44	49	48
16	19	20	25	24	44	45	50	49
17	26	27	32	31	51	52	57	56
18	27	28	33	32	52	53	58	57
19	28	29	34	33	53	54	59	58
20	29	30	35	34	54	55	60	59
21	31	32	37	36	56	57	62	61
22	32	33	38	37	57	58	63	62
23	33	34	39	38	58	59	64	63
24	34	35	40	39	59	60	65	64
25	36	37	42	41	61	62	67	66
26	37	38	43	42	62	63	68	67
27	38	39	44	43	63	64	69	68
28	39	40	45	44	64	65	70	69
29	41	42	47	46	66	67	72	71
30	42	43	48	47	67	68	73	72
31	43	44	49	48	68	69	74	73
32	44	45	50	49	69	70	75	74
33	51	52	57	56	76	77	82	81
34	52	53	58	57	77	78	83	82
35	53	54	59	58	78	79	84	83
36	54	55	60	59	79	80	85	84
37	56	57	62	61	81	82	87	86
38	57	58	63	62	82	83	88	87
39	58	59	64	63	83	84	89	88
40	59	60	65	64	84	85	90	89
41	61	62	67	66	86	87	92	91
42	62	63	68	67	87	88	93	92
43	63	64	69	68	88	89	94	93
44	64	65	70	69	89	90	95	94
45	66	67	72	71	91	92	97	96
46	67	68	73	72	92	93	98	97
47	68	69	74	73	93	94	99	98
48	69	70	75	74	94	95	100	99
49	76	77	82	81	101	102	107	106
50	77	78	83	82	102	103	108	107
51	78	79	84	83	103	104	109	108
52	79	80	85	84	104	105	110	109
53	81	82	87	86	106	107	112	111
54	82	83	88	87	107	108	113	112
55	83	84	89	88	108	109	114	113
56	84	85	90	89	109	110	115	114
57	86	87	92	91	111	112	117	116
58	87	88	93	92	112	113	118	117
59	88	89	94	93	113	114	119	118
60	89	90	95	94	114	115	120	119
61	91	92	97	96	116	117	122	121
62	92	93	98	97	117	118	123	122
63	93	94	99	98	118	119	124	123
64	94	95	100	99	119	120	125	124
0	0	0	0	0	0	0	0	0

stop

Fig. 11. Continued

```

fehm.4.0      12/10/90

***** 3-D Heat Conduction Model (4X4X4 cubes) *****

output file,wt tape,rd tp,user call parameter
  11  44  0  0

storage for geometric coefficients 726,   in common(nr) 48000
pressures and temperatures set by gradients
storage needed for ncon 851,   available 80000
storage needed for nop 851,   available 100000
storage needed for a matrix 725,   available 300000
storage needed for b matrix 725,   available 720000
storage needed for gmres 1125,   available 187200

time for reading input,forming coefficients  7.49

**** analysis of input data on file fe.chk ****

time step      1
      1      2.0      125.0

years      0.137e-04 days  0.5000000e-02 ts size  5.000e-03
cpu sec for step  0.3677e-01 total time  0.7310e-01
node  p(mpa)  e(mj)  l sat  temp(c)  well dis  dis ent  r eq1  r eq2
  1    10.000  0.00  0.000  200.000  0.000e+00  0.000  0.3e-12  0.3e-03
  56   10.000  0.00  0.000  199.929  0.000e+00  0.000  0.4e-07  0.7e-01
  87   10.000  0.00  0.000  197.313  0.000e+00  0.000  0.2e-06  0.3e+01
  94   10.000  0.00  0.000  192.518  0.000e+00  0.000 -0.6e-07  0.7e+01
   5    10.000  0.00  0.000  100.000  0.000e+00  0.000 -0.2e-09  0.1e+03
  25   10.000  0.00  0.000  100.000  0.000e+00  0.000 -0.2e-09  0.1e+03
   2    10.000  0.00  0.000  199.998  0.000e+00  0.000  0.8e-09  0.2e-02
 125   10.000  0.00  0.000  100.000  0.000e+00  0.000 -0.2e-09  0.1e+03

res mass0.000000      kg vap mass0.000000      kq energy-55.8459      mj
net discharge  0.00000      kg net energy discharge  0.00000      mj
conservation errors:mass  0.00000      energy  0.00000

this time step discharges : ,mass,enthalpy,power
      0.000e+00 kg      0.000e+00 mj      0.000e+00 mw

cumulative discharges : ,mass,enthalpy,avg power
      0.000e+00 kg      0.000e+00 mj      0.000e+00 mw
number of region changes this time step 0

```

Fig. 12. Computer output for the 3-D heat conduction example.



```

time step          601
      1          0.0      125.0

years          0.821e-02 days      0.3000050e+01 ts size      5.000e-05
cpu sec for step      0.3268e-01 total time      0.3021e+02
node      p(mpa)      e(mj)      l sat      temp(c)      well dis      dis ent      r eq1      r eq2
  1      10.000      0.00      0.000      100.107      0.000e+00      0.000      -0.5e-11      0.1e-04
  56      10.000      0.00      0.000      100.070      0.000e+00      0.000      0.2e-12      0.9e-05
  87      10.000      0.00      0.000      100.027      0.000e+00      0.000      -0.7e-12      0.3e-05
  94      10.000      0.00      0.000      100.006      0.000e+00      0.000      -0.3e-12      0.8e-06
  5      10.000      0.00      0.000      100.000      0.000e+00      0.000      -0.4e-12      -0.4e-12
  25      10.000      0.00      0.000      100.000      0.000e+00      0.000      -0.8e-25      -0.2e-26
  2      10.000      0.00      0.000      100.099      0.000e+00      0.000      0.5e-14      0.1e-04
  125      10.000      0.00      0.000      100.000      0.000e+00      0.000      0.0e+00      0.1e-38

res mass0.000000      kg vap mass0.000000      kq energy-33.7589      mj
net discharge      0.00000      kg net energy discharge      0.00000      mj
conservation errors:mass      0.00000      energy      0.00000

this time step discharges : ,mass,enthalpy,power
      0.000e+00 kg      0.000e+00 mj      0.000e+00 mw

cumulative discharges : ,mass,enthalpy,avg power
      0.000e+00 kg      0.000e+00 mj      0.000e+00 mw
number of region changes this time step 0

simulation ended: days      3.000e+00 timesteps      601
                  contour plt:fe.con , history plt:fe.his
total newton-raphson iterations= 601

```

Fig. 12. Continued

```
temp plot
08
3 1 1 1 1 1 1 1
0 0 0 0
6.5 6.5
0
0 3. .5 2
0 200.0 20.0 2
temperature vs time in cube
days
temperature(deg c)
```

Fig. 13. Instruction file (HIS.INS) for postprocessor FEHPLTR for the heat conduction problem.

feh4.0 12/10/90 temperature vs time in cube

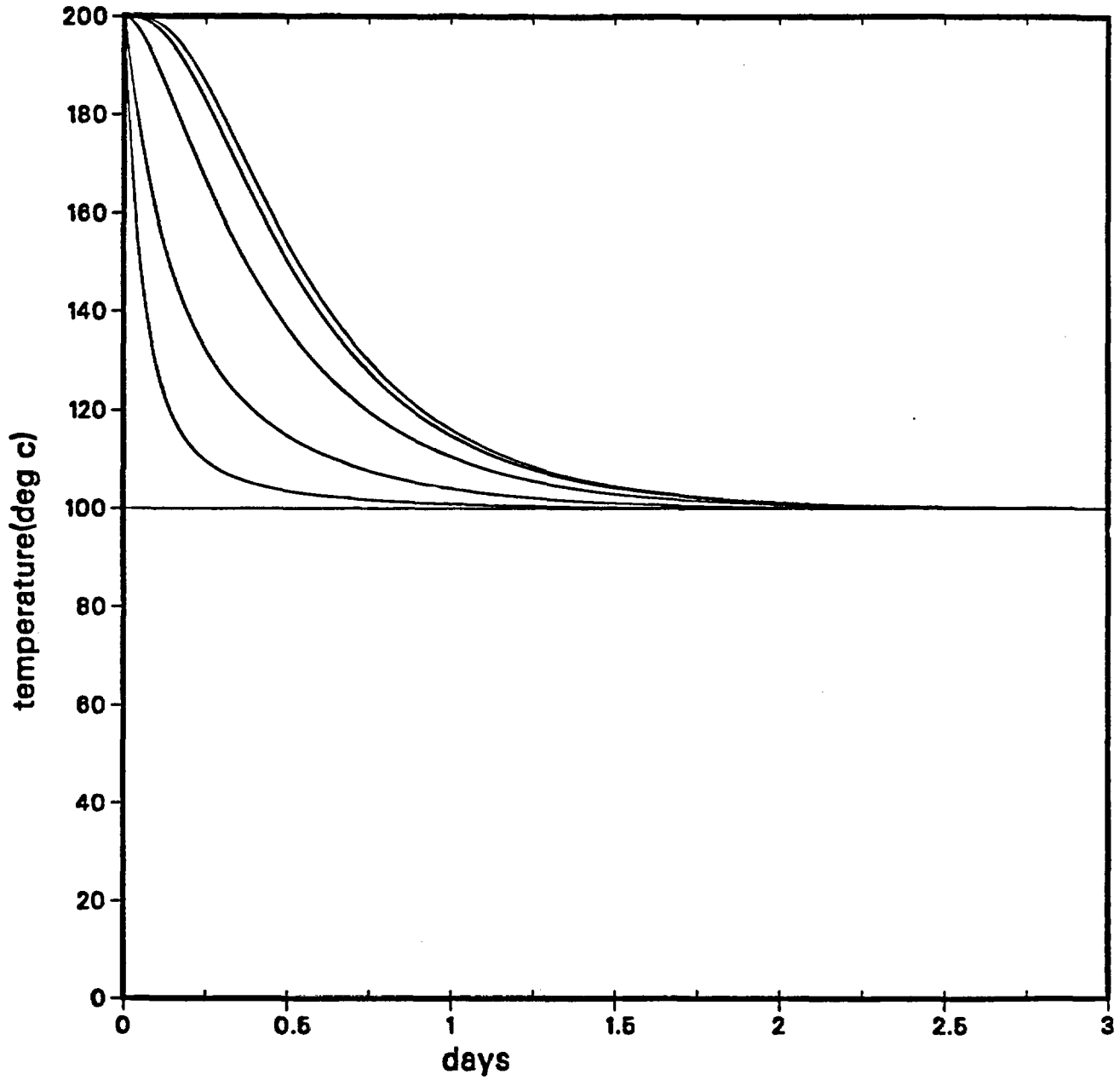


Fig. 14. History plot for the heat conduction problem.

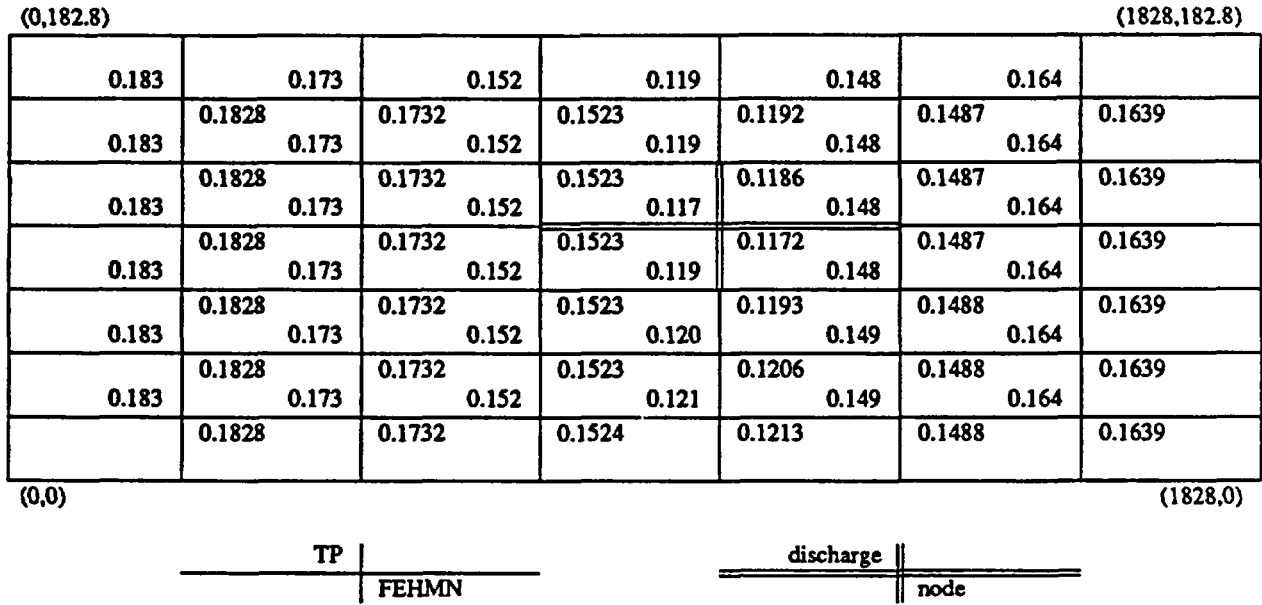


Fig. 15. Solution domain and results for the Toronyi example.

```

2D Model of a Rectangle
4 1 4 0 2 1 0
1 1 2 3 4
O. 1828. 1828. 0.
O. 0. 182.8 182.8
1 07 07 1
.5 1 1 1 1 1 .5
.5 1 1 1 1 1 .5

```

Fig. 16. Input for GENMSH for the Toronyi example.

```

**** toronyi example ****
node
  36
  10 11 12 13 14 15
  18 19 20 21 22 23
  26 27 28 29 30 31
  34 35 36 37 38 39
  42 43 44 45 46 47
  50 51 52 53 54 55
sol
  1 -1
init
  4.3000 000. 250. 0. 0. 250. 0. 0.
rip
  2 0.05 0.05 1.0 1.0
  0
  1 64 1 1
  0 0 0 0 0
pres
  1 64 1 4.3000 .2 2
  0 0 0 0. 0. 0
rock
  1 64 1 2563. 1010. 0.0500 1.0000
  0 0 0 0. 0. 0. 0.
cond
  1 64 01 1.73e-00 1.73e-00 0.0e-00
  0 0 0 0. 0. 0.
perm
  1 64 1 9.869e-13 9.869e-13 0.e-00 0. 0. 0.
  0 0 0 0. 0. 0. 0. 0. 0.
flow
  029 029 1 0.082011 -025. 0.
  0 0 0 0. 0. 0
time
  8.3 78.3 0009 10 1985 07
  8.3 10. 1.0 10
  0. 0. 0. 0
ctrl
  40 1.e-8 08
  1 64 1 1
  0 0 0 0
  40 1.0 0.0 0.75
  1 0 1.00 0.0001 010.00
coord
  64
      1 0.00000 182.80000 0.00000
      2 152.33333 182.80000 0.00000
      3 457.00000 182.80000 0.00000
      4 761.66667 182.80000 0.00000
      5 1066.33333 182.80000 0.00000
      6 1371.00000 182.80000 0.00000
      7 1675.66667 182.80000 0.00000
      8 1828.00000 182.80000 0.00000
      9 0.00000 167.56667 0.00000
     10 152.33333 167.56667 0.00000
     11 457.00000 167.56667 0.00000
     12 761.66667 167.56667 0.00000
     13 1066.33333 167.56667 0.00000
     14 1371.00000 167.56667 0.00000
     15 1675.66667 167.56667 0.00000
     16 1828.00000 167.56667 0.00000
     17 0.00000 137.10000 0.00000
     18 152.33333 137.10000 0.00000
     19 457.00000 137.10000 0.00000
     20 761.66667 137.10000 0.00000
     21 1066.33333 137.10000 0.00000
     22 1371.00000 137.10000 0.00000
     23 1675.66667 137.10000 0.00000
     24 1828.00000 137.10000 0.00000
     25 0.00000 106.63333 0.00000

```

Fig. 17. Input file for FEHMN for Toronyi example.

26	152.33333	106.63333	0.00000
27	457.00000	106.63333	0.00000
28	761.66667	106.63333	0.00000
29	1066.33333	106.63333	0.00000
30	1371.00000	106.63333	0.00000
31	1675.66667	106.63333	0.00000
32	1828.00000	106.63333	0.00000
33	0.00000	76.16667	0.00000
34	152.33333	76.16667	0.00000
35	457.00000	76.16667	0.00000
36	761.66667	76.16667	0.00000
37	1066.33333	76.16667	0.00000
38	1371.00000	76.16667	0.00000
39	1675.66667	76.16667	0.00000
40	1828.00000	76.16667	0.00000
41	0.00000	45.70000	0.00000
42	152.33333	45.70000	0.00000
43	457.00000	45.70000	0.00000
44	761.66667	45.70000	0.00000
45	1066.33333	45.70000	0.00000
46	1371.00000	45.70000	0.00000
47	1675.66667	45.70000	0.00000
48	1828.00000	45.70000	0.00000
49	0.00000	15.23333	0.00000
50	152.33333	15.23333	0.00000
51	457.00000	15.23333	0.00000
52	761.66667	15.23333	0.00000
53	1066.33333	15.23333	0.00000
54	1371.00000	15.23333	0.00000
55	1675.66667	15.23333	0.00000
56	1828.00000	15.23333	0.00000
57	0.00000	0.00000	0.00000
58	152.33333	0.00000	0.00000
59	457.00000	0.00000	0.00000
60	761.66667	0.00000	0.00000
61	1066.33333	0.00000	0.00000
62	1371.00000	0.00000	0.00000
63	1675.66667	0.00000	0.00000
64	1828.00000	0.00000	0.00000
0	0.00000	0.00000	0.00000

elem		0		2		1	
4,	49,						
1	9	10	2	1			
2	10	11	3	2			
3	11	12	4	3			
4	12	13	5	4			
5	13	14	6	5			
6	14	15	7	6			
7	15	16	8	7			
8	17	18	10	9			
9	18	19	11	10			
10	19	20	12	11			
11	20	21	13	12			
12	21	22	14	13			
13	22	23	15	14			
14	23	24	16	15			
15	25	26	18	17			
16	26	27	19	18			
17	27	28	20	19			
18	28	29	21	20			
19	29	30	22	21			
20	30	31	23	22			
21	31	32	24	23			
22	33	34	26	25			
23	34	35	27	26			
24	35	36	28	27			
25	36	37	29	28			

Fig. 17. (Continued)

26	37	38	30	29
27	38	39	31	30
28	39	40	32	31
29	41	42	34	33
30	42	43	35	34
31	43	44	36	35
32	44	45	37	36
33	45	46	38	37
34	46	47	39	38
35	47	48	40	39
36	49	50	42	41
37	50	51	43	42
38	51	52	44	43
39	52	53	45	44
40	53	54	46	45
41	54	55	47	46
42	55	56	48	47
43	57	58	50	49
44	58	59	51	50
45	59	60	52	51
46	60	61	53	52
47	61	62	54	53
48	62	63	55	54
49	63	64	56	55
0	0	0	0	0

stop

Fig. 17. Continued.

feh.4.0 12/11/90

\*\*\*\* toronyi example \*\*\*\*

output file,wt tape,rd tp,user call parameter  
12 44 0 0

storage for geometric coefficients 218, in common(nr) 48000  
pressures and temperatures set by gradients  
storage needed for ncon 353, available 80000  
storage needed for nop 353, available 100000  
storage needed for a matrix 1152, available 300000  
storage needed for b matrix 1152, available 720000  
storage needed for gmres 1152, available 187200

time for reading input,forming coefficients 6.94

\*\*\*\* analysis of input data on file fe.chk \*\*\*\*

time step 1

3 8.0 64.0

years 0.227e-01 days 0.830000e+01 ts size 8.300e+00

cpu sec for step 0.1750e+00 total time 0.2091e+00

node	p(mpa)	e(mj)	l sat	temp(c)	well dis	dis ent	r eq1	r eq2
10	4.300	1.27	0.200	254.600	0.000e+00	0.000	-0.3e-12	-0.7e-13
11	4.299	1.27	0.199	254.585	0.000e+00	0.000	-0.2e-12	-0.2e-12
12	4.293	1.28	0.196	254.507	0.000e+00	0.000	-0.2e-11	-0.1e-11
13	4.265	1.29	0.182	254.123	0.000e+00	0.000	0.3e-11	-0.7e-12
14	4.293	1.28	0.196	254.506	0.000e+00	0.000	0.4e-11	0.2e-11
15	4.298	1.27	0.199	254.580	0.000e+00	0.000	-0.9e-12	-0.4e-12
18	4.300	1.27	0.200	254.600	0.000e+00	0.000	-0.1e-11	-0.6e-12
19	4.299	1.27	0.199	254.585	0.000e+00	0.000	-0.4e-12	-0.2e-12
20	4.293	1.28	0.196	254.507	0.000e+00	0.000	-0.6e-11	-0.3e-11
21	4.264	1.29	0.181	254.101	0.000e+00	0.000	0.3e-12	0.2e-12
22	4.293	1.28	0.196	254.506	0.000e+00	0.000	0.2e-10	0.9e-11
23	4.298	1.27	0.199	254.580	0.000e+00	0.000	-0.3e-11	-0.2e-11
26	4.300	1.27	0.200	254.600	0.000e+00	0.000	-0.1e-11	-0.6e-12
27	4.299	1.27	0.199	254.585	0.000e+00	0.000	-0.2e-12	-0.1e-12
28	4.293	1.28	0.196	254.507	0.000e+00	0.000	0.7e-11	0.4e-11
29	4.261	1.29	0.179	254.055	0.820e-01	2.792	-0.4e-12	0.2e-11
30	4.293	1.28	0.196	254.506	0.000e+00	0.000	0.8e-11	0.4e-11
31	4.298	1.27	0.199	254.580	0.000e+00	0.000	-0.5e-11	-0.3e-11
34	4.300	1.27	0.200	254.600	0.000e+00	0.000	-0.1e-11	-0.5e-12
35	4.299	1.27	0.199	254.585	0.000e+00	0.000	0.8e-13	0.1e-12
36	4.293	1.28	0.196	254.508	0.000e+00	0.000	0.2e-10	0.8e-11
37	4.265	1.29	0.182	254.118	0.000e+00	0.000	0.4e-13	0.2e-12
38	4.293	1.28	0.196	254.507	0.000e+00	0.000	-0.8e-11	-0.4e-11
39	4.298	1.27	0.199	254.580	0.000e+00	0.000	-0.5e-11	-0.3e-11
42	4.300	1.27	0.200	254.600	0.000e+00	0.000	-0.1e-11	-0.7e-12
43	4.299	1.27	0.199	254.585	0.000e+00	0.000	-0.3e-12	-0.3e-12
44	4.293	1.28	0.196	254.508	0.000e+00	0.000	0.7e-11	0.4e-11
45	4.268	1.29	0.183	254.158	0.000e+00	0.000	0.2e-12	-0.6e-12
46	4.293	1.28	0.196	254.507	0.000e+00	0.000	-0.1e-10	-0.6e-11
47	4.298	1.27	0.199	254.580	0.000e+00	0.000	-0.5e-11	-0.3e-11
50	4.300	1.27	0.200	254.600	0.000e+00	0.000	-0.7e-12	-0.4e-12
51	4.299	1.27	0.199	254.585	0.000e+00	0.000	-0.4e-12	-0.2e-12
52	4.293	1.28	0.196	254.509	0.000e+00	0.000	-0.6e-11	-0.3e-11
53	4.269	1.29	0.174	254.178	0.000e+00	0.000	-0.2e-12	-0.5e-12
54	4.293	1.28	0.196	254.508	0.000e+00	0.000	-0.7e-11	-0.3e-11
55	4.298	1.27	0.199	254.580	0.000e+00	0.000	-0.3e-11	-0.2e-11

res mass 0.287727e+07 kg vap mass 290027. kq energy 0.212729e+09 mj

net discharge 58812. kg net energy discharge 0.16422e+06 mj  
conservation errors:mass -0.66302e-08 energy -0.66939e-08

this time step discharges : ,mass,enthalpy,power  
5.881e+04 kg 1.642e+05 mj 2.290e-01 mw

cumulative discharges : ,mass,enthalpy,avg power  
5.881e+04 kg 1.642e+05 mj 2.290e-01 mw  
number of region changes this time step 0

Fig. 18. Output for the Toronyi example.



```

time step          9
      1          1.0          64.0

years          0.214e+00 days          0.7830010e-02 ts size          1.000e-04
cpu sec for step          0.5129e-01 total time          0.1539e+01
node      p(mpa)      e(mj)      l sat      temp(c)      well dis      dis ent      r eq1      r eq2
10      4.267      1.29      0.183      254.151      0.000e+00      0.000      0.3e-13      0.4e-14
11      4.249      1.30      0.173      253.895      0.000e+00      0.000      -0.2e-13      -0.2e-14
12      4.209      1.32      0.153      253.336      0.000e+00      0.000      0.2e-12      -0.5e-14
13      4.146      1.37      0.120      252.441      0.000e+00      0.000      0.4e-13      0.5e-16
14      4.203      1.32      0.149      253.242      0.000e+00      0.000      0.7e-13      -0.3e-14
15      4.232      1.31      0.164      253.650      0.000e+00      0.000      0.3e-13      -0.5e-14
18      4.267      1.29      0.183      254.151      0.000e+00      0.000      -0.7e-13      -0.9e-15
19      4.249      1.30      0.173      253.895      0.000e+00      0.000      -0.2e-13      0.5e-14
20      4.209      1.32      0.153      253.336      0.000e+00      0.000      -0.7e-13      -0.2e-15
21      4.145      1.37      0.119      252.421      0.000e+00      0.000      -0.9e-13      -0.5e-14
22      4.203      1.32      0.149      253.242      0.000e+00      0.000      -0.7e-13      0.8e-14
23      4.232      1.31      0.164      253.650      0.000e+00      0.000      -0.1e-12      -0.5e-15
26      4.267      1.29      0.183      254.151      0.000e+00      0.000      0.5e-13      -0.7e-14
27      4.249      1.30      0.173      253.895      0.000e+00      0.000      0.5e-13      0.5e-14
28      4.209      1.32      0.153      253.336      0.000e+00      0.000      -0.3e-14      0.2e-14
29      4.142      1.38      0.118      252.382      0.820e-01      2.799      -0.6e-13      -0.2e-14
30      4.203      1.32      0.149      253.242      0.000e+00      0.000      0.7e-14      -0.6e-14
31      4.232      1.31      0.164      253.650      0.000e+00      0.000      -0.5e-13      -0.1e-13
34      4.267      1.29      0.183      254.151      0.000e+00      0.000      -0.5e-13      0.4e-14
35      4.249      1.30      0.173      253.895      0.000e+00      0.000      -0.1e-13      -0.9e-15
36      4.210      1.32      0.153      253.337      0.000e+00      0.000      -0.1e-13      0.1e-14
37      4.146      1.37      0.120      252.439      0.000e+00      0.000      -0.1e-13      0.7e-14
38      4.203      1.32      0.149      253.243      0.000e+00      0.000      0.8e-14      -0.7e-14
39      4.232      1.31      0.164      253.650      0.000e+00      0.000      0.8e-13      -0.3e-14
42      4.267      1.29      0.183      254.151      0.000e+00      0.000      -0.3e-13      -0.4e-14
43      4.249      1.30      0.173      253.895      0.000e+00      0.000      0.1e-13      0.6e-14
44      4.210      1.32      0.153      253.338      0.000e+00      0.000      0.4e-13      -0.9e-15
45      4.149      1.37      0.121      252.477      0.000e+00      0.000      -0.7e-13      0.4e-15
46      4.203      1.32      0.149      253.243      0.000e+00      0.000      0.5e-13      0.4e-14
47      4.232      1.31      0.164      253.650      0.000e+00      0.000      0.1e-12      -0.5e-14
50      4.267      1.29      0.183      254.151      0.000e+00      0.000      -0.2e-13      -0.8e-15
51      4.249      1.30      0.173      253.895      0.000e+00      0.000      0.8e-13      -0.1e-14
52      4.210      1.32      0.153      253.339      0.000e+00      0.000      0.2e-12      0.2e-14
53      4.150      1.37      0.122      252.496      0.000e+00      0.000      0.4e-13      0.5e-14
54      4.203      1.32      0.149      253.244      0.000e+00      0.000      -0.1e-12      -0.4e-15
55      4.232      1.31      0.164      253.650      0.000e+00      0.000      -0.7e-13      -0.7e-15

res mass0.238127e+07 kg vap mass 298427.      kq energy0.211341e+09 mj
net discharge      0.55481e+06 kg net energy discharge      0.15518e+07 mj
conservation errors:mass      -0.29266e-08 energy      -0.43337e-08

this time step discharges : ,mass,enthalpy,power
7.086e-01 kg      1.983e+00 mj      2.295e-01 mw

cumulative discharges : ,mass,enthalpy,avg power
5.548e+05 kg      1.552e+06 mj      2.294e-01 mw
number of region changes this time step 0

simulation ended: days 7.830e+01 timesteps      9
contour plt:fe.con , history plt:fe.his
total newton-raphson iterations- 19

```

Fig. 18. (Continued)

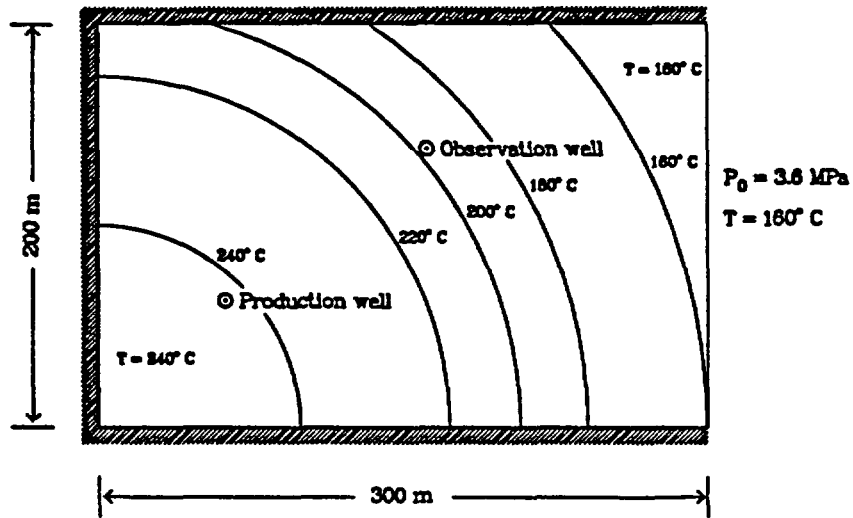


Fig. 19. Schematic diagram of the geometry and boundary conditions for the DOE code comparison project problem.

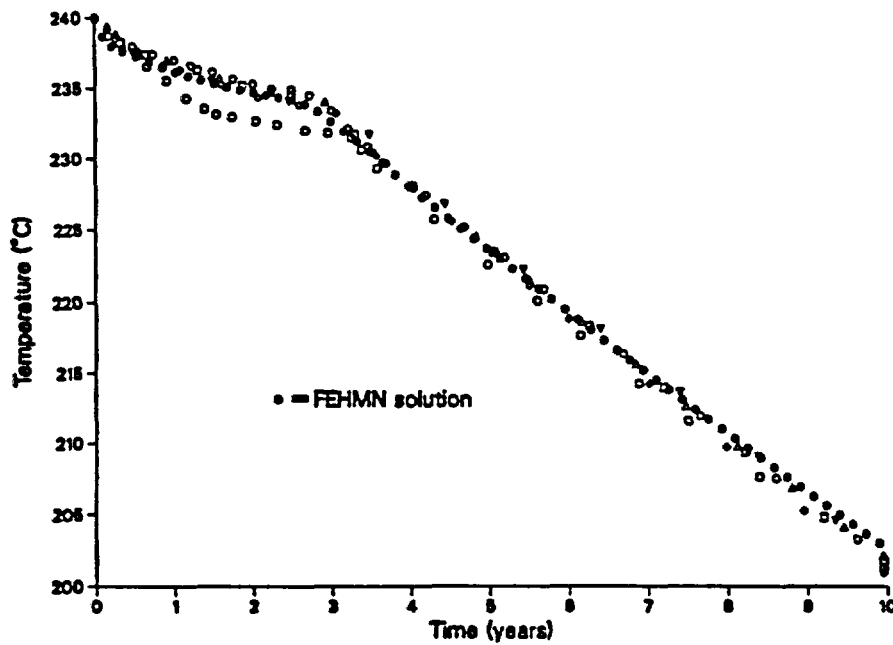


Fig. 20. Comparison of FEHMN production well temperatures with results from other codes.

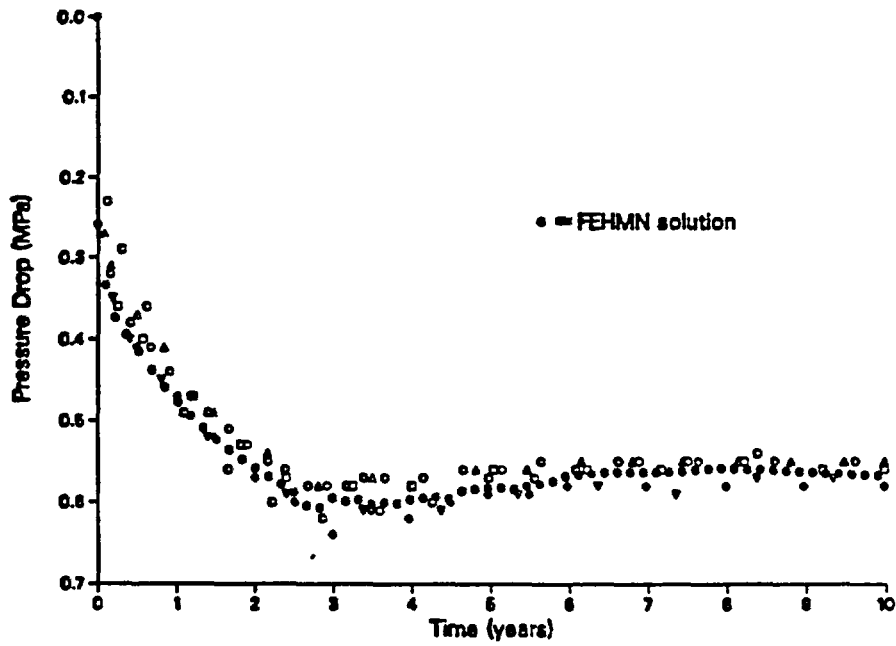


Fig. 21. Comparison of FEHMN production well pressure with results from other codes.

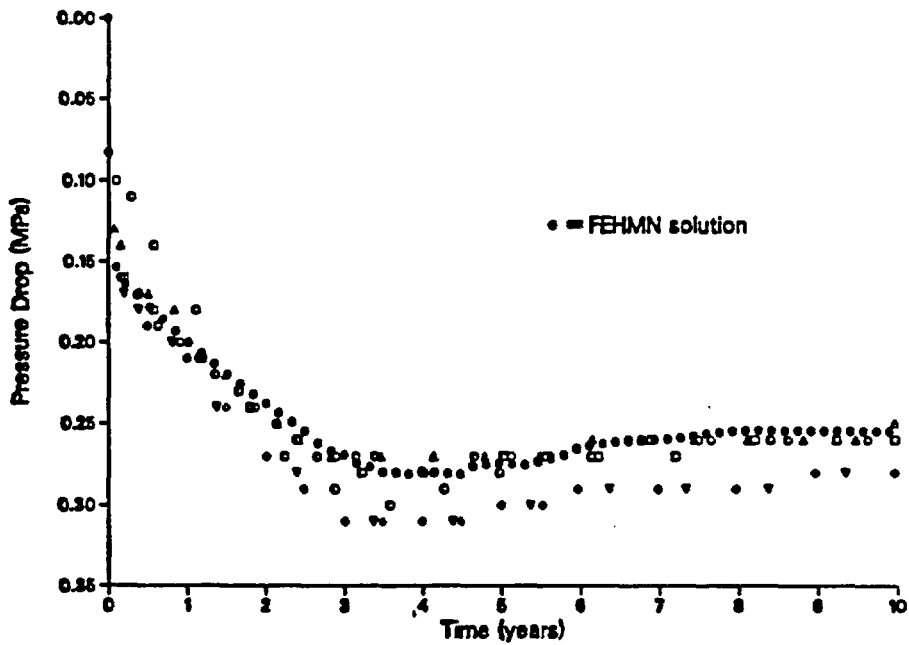


Fig. 22. Comparison of FEHMN observation well pressure with results from other codes.

```

DOE Code Comparison Project, Problem 5, Case A
8 1 8 0 2 1 0
1 1 2 3 4 5 6 7 8
0. 150. 300. 300. 300. 150. 0. 0.
0. 0. 0. 100. 200. 200. 200. 100.
1 13 9 1
.5 1 1 1 1 1 1 1 1 1 1 .5
.5 1 1 1 1 1 1 1 .5

```

Fig. 23. Input for GENMSH for the DOE example.

```

*** DOE Code Comparison Project, Problem 5, Case A ***
node
2
88 50
sol
  1    1
init
  3.6000    0.00    240.    0.    0.    240.    0.    0.
rlp
  2    0.3    0.1    0.0    0.0
0
1 140 1 1
0 0 0 0
rock
  1    140    1    2563.    1010.    0.3500
  0     0     0     0.     0.     0.
cond
  1    140    1    1.00e-00    1.00e-00    0.00e-00
  0     0     0    0.00e-00    0.00e-00    0.00e-00
perm
  1    140    1    2.50e-14    2.50e-14    0.00e-00
  0     0     0    0.00e-00    0.00e-00    0.00e-00
flow
  88    88    1    0.050    -25.    0.
  14   140   14    3.600    -160.0    1.
  0     0     0     0.     0.     0.

```

Fig. 24. Input for FEHMN for the DOE example.

```

time
 30.0    3650.    10000    1000    1989    10
1.0 -1.2  1.0 1000
  0.    0.    0.    0
ctrl
 40    1.e-7    8
  1    140    1    1
  0    0    0    0
 1.0    0.0    1.00
 40    1.2    .1    60.000
  1    0
coor
140
  1      0.00000    200.00000    0.00000
  2     12.50000    200.00000    0.00000
  3     37.50000    200.00000    0.00000
  4     62.50000    200.00000    0.00000
  5     87.50000    200.00000    0.00000
  6    112.50000    200.00000    0.00000
  7    137.50000    200.00000    0.00000
  8    162.50000    200.00000    0.00000
  9    187.50000    200.00000    0.00000
 10    212.50000    200.00000    0.00000
 11    237.50000    200.00000    0.00000
 12    262.50000    200.00000    0.00000
 13    287.50000    200.00000    0.00000
 14    300.00000    200.00000    0.00000
 15      0.00000    187.50000    0.00000
 16     12.50000    187.50000    0.00000
 17     37.50000    187.50000    0.00000
 18     62.50000    187.50000    0.00000
 19     87.50000    187.50000    0.00000
 20    112.50000    187.50000    0.00000
 21    137.50000    187.50000    0.00000
 22    162.50000    187.50000    0.00000
 23    187.50000    187.50000    0.00000
 24    212.50000    187.50000    0.00000
 25    237.50000    187.50000    0.00000
 26    262.50000    187.50000    0.00000
 27    287.50000    187.50000    0.00000
 28    300.00000    187.50000    0.00000
 29      0.00000    162.50000    0.00000
 30     12.50000    162.50000    0.00000
 31     37.50000    162.50000    0.00000
 32     62.50000    162.50000    0.00000
 33     87.50000    162.50000    0.00000
 34    112.50000    162.50000    0.00000
 35    137.50000    162.50000    0.00000
 36    162.50000    162.50000    0.00000
 37    187.50000    162.50000    0.00000
 38    212.50000    162.50000    0.00000
 39    237.50000    162.50000    0.00000
 40    262.50000    162.50000    0.00000
 41    287.50000    162.50000    0.00000
 42    300.00000    162.50000    0.00000
 43      0.00000    137.50000    0.00000
 44     12.50000    137.50000    0.00000
 45     37.50000    137.50000    0.00000

```

Fig. 24. (continued)

46	62.50000	137.50000	0.00000
47	87.50000	137.50000	0.00000
48	112.50000	137.50000	0.00000
49	137.50000	137.50000	0.00000
50	162.50000	137.50000	0.00000
51	187.50000	137.50000	0.00000
52	212.50000	137.50000	0.00000
53	237.50000	137.50000	0.00000
54	262.50000	137.50000	0.00000
55	287.50000	137.50000	0.00000
56	300.00000	137.50000	0.00000
57	0.00000	112.50000	0.00000
58	12.50000	112.50000	0.00000
59	37.50000	112.50000	0.00000
60	62.50000	112.50000	0.00000
61	87.50000	112.50000	0.00000
62	112.50000	112.50000	0.00000
63	137.50000	112.50000	0.00000
64	162.50000	112.50000	0.00000
65	187.50000	112.50000	0.00000
66	212.50000	112.50000	0.00000
67	237.50000	112.50000	0.00000
68	262.50000	112.50000	0.00000
69	287.50000	112.50000	0.00000
70	300.00000	112.50000	0.00000
71	0.00000	87.50000	0.00000
72	12.50000	87.50000	0.00000
73	37.50000	87.50000	0.00000
74	62.50000	87.50000	0.00000
75	87.50000	87.50000	0.00000
76	112.50000	87.50000	0.00000
77	137.50000	87.50000	0.00000
78	162.50000	87.50000	0.00000
79	187.50000	87.50000	0.00000
80	212.50000	87.50000	0.00000
81	237.50000	87.50000	0.00000
82	262.50000	87.50000	0.00000
83	287.50000	87.50000	0.00000
84	300.00000	87.50000	0.00000
85	0.00000	62.50000	0.00000
86	12.50000	62.50000	0.00000
87	37.50000	62.50000	0.00000
88	62.50000	62.50000	0.00000
89	87.50000	62.50000	0.00000
90	112.50000	62.50000	0.00000
91	137.50000	62.50000	0.00000
92	162.50000	62.50000	0.00000
93	187.50000	62.50000	0.00000
94	212.50000	62.50000	0.00000
95	237.50000	62.50000	0.00000
96	262.50000	62.50000	0.00000
97	287.50000	62.50000	0.00000
98	300.00000	62.50000	0.00000
99	0.00000	37.50000	0.00000
100	12.50000	37.50000	0.00000
101	37.50000	37.50000	0.00000
102	62.50000	37.50000	0.00000

Fig. 24. (continued)

103	87.50000	37.50000	0.00000
104	112.50000	37.50000	0.00000
105	137.50000	37.50000	0.00000
106	162.50000	37.50000	0.00000
107	187.50000	37.50000	0.00000
108	212.50000	37.50000	0.00000
109	237.50000	37.50000	0.00000
110	262.50000	37.50000	0.00000
111	287.50000	37.50000	0.00000
112	300.00000	37.50000	0.00000
113	0.00000	12.50000	0.00000
114	12.50000	12.50000	0.00000
115	37.50000	12.50000	0.00000
116	62.50000	12.50000	0.00000
117	87.50000	12.50000	0.00000
118	112.50000	12.50000	0.00000
119	137.50000	12.50000	0.00000
120	162.50000	12.50000	0.00000
121	187.50000	12.50000	0.00000
122	212.50000	12.50000	0.00000
123	237.50000	12.50000	0.00000
124	262.50000	12.50000	0.00000
125	287.50000	12.50000	0.00000
126	300.00000	12.50000	0.00000
127	0.00000	0.00000	0.00000
128	12.50000	0.00000	0.00000
129	37.50000	0.00000	0.00000
130	62.50000	0.00000	0.00000
131	87.50000	0.00000	0.00000
132	112.50000	0.00000	0.00000
133	137.50000	0.00000	0.00000
134	162.50000	0.00000	0.00000
135	187.50000	0.00000	0.00000
136	212.50000	0.00000	0.00000
137	237.50000	0.00000	0.00000
138	262.50000	0.00000	0.00000
139	287.50000	0.00000	0.00000
140	300.00000	0.00000	0.00000
0	0.00000	0.00000	0.00000

elem

4 117 0

1	15	16	2	1
2	16	17	3	2
3	17	18	4	3
4	18	19	5	4
5	19	20	6	5
6	20	21	7	6
7	21	22	8	7
8	22	23	9	8
9	23	24	10	9
10	24	25	11	10
11	25	26	12	11
12	26	27	13	12
13	27	28	14	13
14	29	30	16	15
15	30	31	17	16
16	31	32	18	17

Fig. 24. (continued)

17	32	33	19	18
18	33	34	20	19
19	34	35	21	20
20	35	36	22	21
21	36	37	23	22
22	37	38	24	23
23	38	39	25	24
24	39	40	26	25
25	40	41	27	26
26	41	42	28	27
27	43	44	30	29
28	44	45	31	30
29	45	46	32	31
30	46	47	33	32
31	47	48	34	33
32	48	49	35	34
33	49	50	36	35
34	50	51	37	36
35	51	52	38	37
36	52	53	39	38
37	53	54	40	39
38	54	55	41	40
39	55	56	42	41
40	57	58	44	43
41	58	59	45	44
42	59	60	46	45
43	60	61	47	46
44	61	62	48	47
45	62	63	49	48
46	63	64	50	49
47	64	65	51	50
48	65	66	52	51
49	66	67	53	52
50	67	68	54	53
51	68	69	55	54
52	69	70	56	55
53	71	72	58	57
54	72	73	59	58
55	73	74	60	59
56	74	75	61	60
57	75	76	62	61
58	76	77	63	62
59	77	78	64	63
60	78	79	65	64
61	79	80	66	65
62	80	81	67	66
63	81	82	68	67
64	82	83	69	68
65	83	84	70	69
66	85	86	72	71
67	86	87	73	72
68	87	88	74	73
69	88	89	75	74
70	89	90	76	75
71	90	91	77	76
72	91	92	78	77
73	92	93	79	78

Fig. 24. (continued)



74	93	94	80	79
75	94	95	81	80
76	95	96	82	81
77	96	97	83	82
78	97	98	84	83
79	99	100	86	85
80	100	101	87	86
81	101	102	88	87
82	102	103	89	88
83	103	104	90	89
84	104	105	91	90
85	105	106	92	91
86	106	107	93	92
87	107	108	94	93
88	108	109	95	94
89	109	110	96	95
90	110	111	97	96
91	111	112	98	97
92	113	114	100	99
93	114	115	101	100
94	115	116	102	101
95	116	117	103	102
96	117	118	104	103
97	118	119	105	104
98	119	120	106	105
99	120	121	107	106
100	121	122	108	107
101	122	123	109	108
102	123	124	110	109
103	124	125	111	110
104	125	126	112	111
105	127	128	114	113
106	128	129	115	114
107	129	130	116	115
108	130	131	117	116
109	131	132	118	117
110	132	133	119	118
111	133	134	120	119
112	134	135	121	120
113	135	136	122	121
114	136	137	123	122
115	137	138	124	123
116	138	139	125	124
117	139	140	126	125
0	0	0	0	0
stop				

Fig. 24. (continued)

fehmn.4.0 12/11/90

\*\*\* DOE Code Comparison Project, Problem 5, Case A \*\*\*

output file,wt tape,rd tp,user call parameter  
13 44 0 0

storage for geometric coefficients 170, in common(nr) 48000  
pressures and temperatures set by gradients  
storage needed for ncon 1261, available 80000  
storage needed for nop 1261, available 100000  
storage needed for a matrix 4480, available 300000  
storage needed for b matrix 4480, available 720000  
storage needed for gmres 2520, available 187200

time for reading input,forming coefficients 7.31

\*\*\*\* analysis of input data on file fe.chk \*\*\*\*

time step 1

4 16.7 140.0

years 0.274e-02 days 0.1000000e+01 ts size 1.000e+00  
cpu sec for step 0.7846e+00 total time 0.8199e+00  
node p(mpa) e(mj) l sat temp(c) well dis dis ent r eq1 r eq2  
46 3.341 1.04 0.999 239.971 0.500e-01 1.037 -0.2e-09 0.5e-10  
92 3.529 1.04 1.000 239.993 0.000e+00 0.000 0.4e-11 -0.8e-12

res mass0.170833e+08 kg vap mass 5.06828 kq energy0.418642e+08 mj

net discharge 2633.7 kg net energy discharge 3335.4 mj  
conservation errors:mass 0.20321 energy 0.24829

this time step discharges : ,mass,enthalpy,power  
4.320e+03 kg 4.478e+03 mj 5.183e-02 mw

cumulative discharges : ,mass,enthalpy,avg power  
4.320e+03 kg 4.478e+03 mj 5.183e-02 mw  
number of region changes this time step 0

time step 63

3 10.3 140.0

years 0.999e+01 days 0.3650000e+04 ts size 3.796e+01  
cpu sec for step 0.4888e+00 total time 0.3765e+02  
node p(mpa) e(mj) l sat temp(c) well dis dis ent r eq1 r eq2  
46 3.015 1.02 0.783 234.252 0.500e-01 1.016 0.3e-11 -0.6e-11  
92 3.353 0.93 1.000 218.169 0.000e+00 0.000 0.1e-11 0.4e-10

res mass0.169256e+08 kg vap mass 19184.9 kq energy0.360994e+08 mj

net discharge 0.16031e+06 kg net energy discharge 0.57681e+07 mj  
conservation errors:mass 0.54996e-04 energy 0.67599e-04

this time step discharges : ,mass,enthalpy,power  
1.640e+05 kg 1.667e+05 mj 5.082e-02 mw

cumulative discharges : ,mass,enthalpy,avg power  
1.577e+07 kg 1.634e+07 mj 5.182e-02 mw  
number of region changes this time step 0

simulation ended: days 3.650e+03 timesteps 63  
contour plt:fe.con , history plt:fe.his  
total newton-raphson iterations= 211

Fig. 25. Output from FEHMN for the DOE problem.

```
2
temp contours for doe problem
0 0
0 300 0 200
0 0
6.5 6.5
1 -1. 0.0 0.0 0.0
8 160. 180. 200. 210. 220. 225. 230. 235.
```

Fig. 26. Instruction file (CON.INS) for the postprocessor FECPLTR for the DOE problem.

temperatures

time= 10.000 years liquid phase temp contours for doe problem

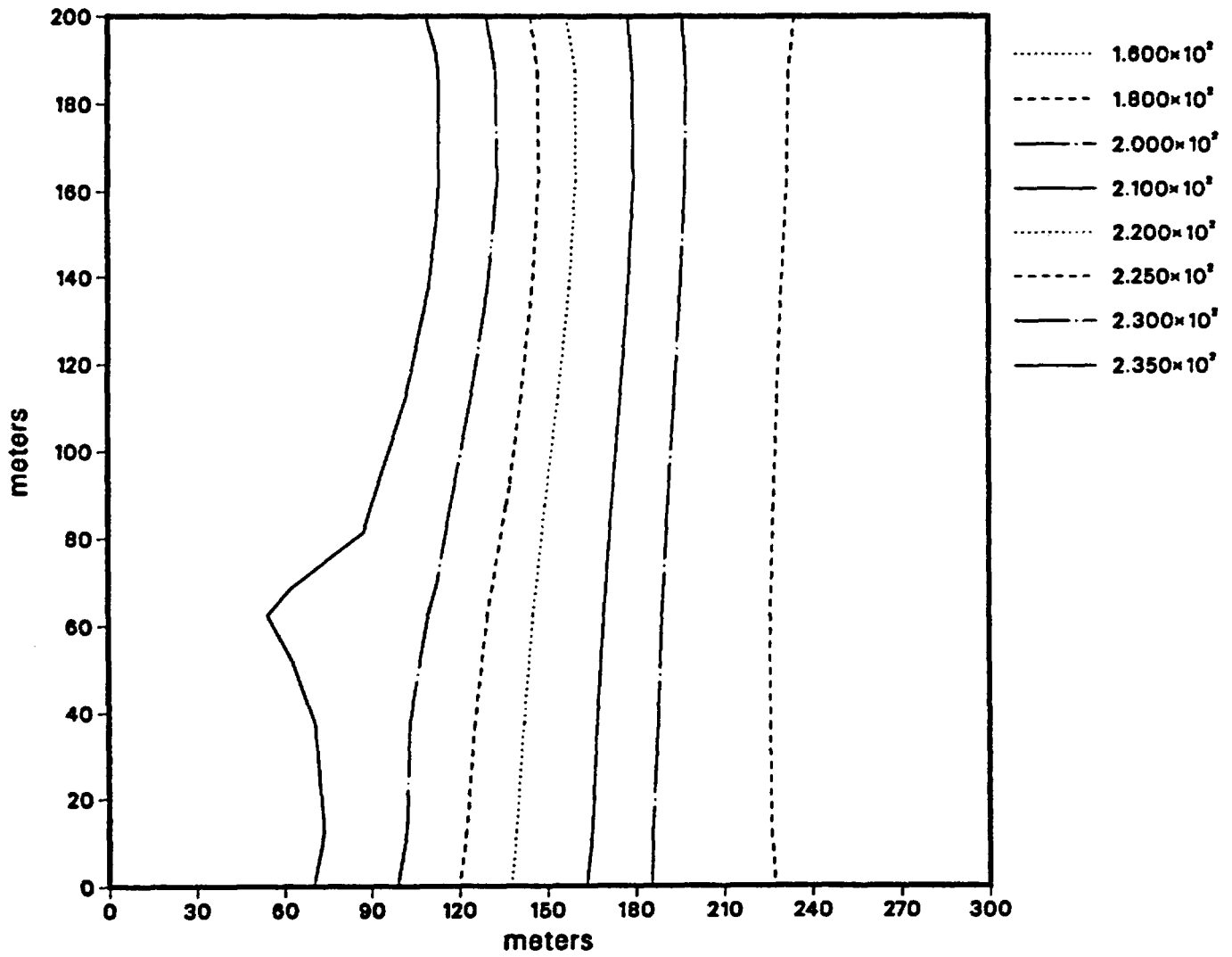


Fig. 27. Contour plot of temperature for the DOE problem.

## ACKNOWLEDGMENTS

The authors thank Kay Coen, Kay Birdsell, and Mary Ann Olson for their contributions to this document.

## DISCLAIMER

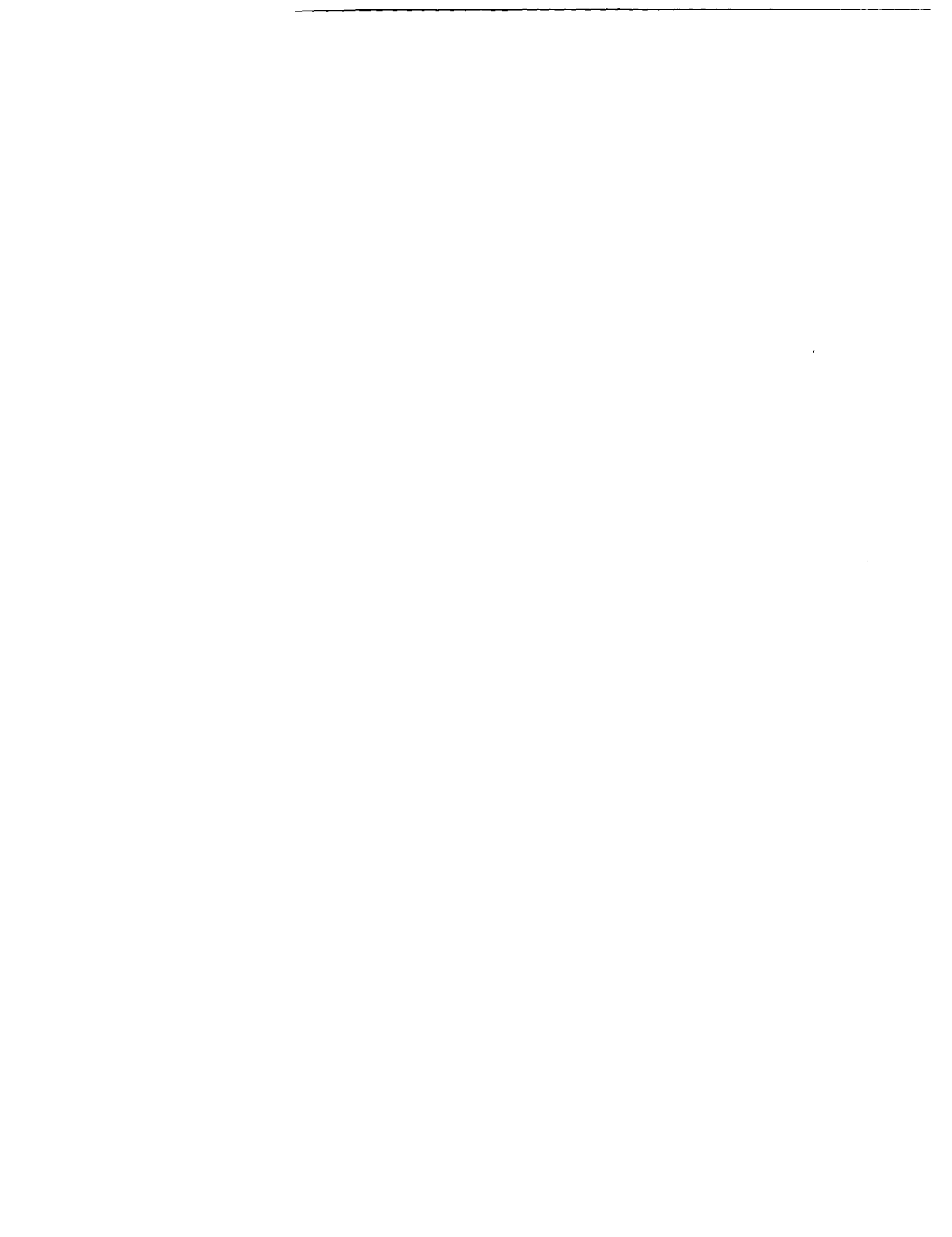
The software documented in this report was not verified, validated, or otherwise subjected to the controls of a Yucca Mountain Site Characterization Project Office-approved quality program.

## REFERENCES

- Behie, A., and P. A. Forsythe, "Incomplete Factorization Methods for Fully Implicit Simulation for Enhanced Oil Recovery," *SIAM, J. Sci. Stat. Comput.* **5**, 543-561 (1984). [NNA.910806.0004].
- Behie, A., and P. K. W. Vinsome, "Block Iterative Methods for Fully Implicit Reservoir Simulations," *Soc. Pet. Eng. J.* **22**, 658-668 (1982). [NNA.910806.0005].
- Birdsell, K. H., K. Campbell, K. G. Eggert, and B. J. Travis, "Simulation of Radionuclide Retardation at Yucca Mountain Using a Stochastic Mineralogical/Geochemical Model," *Proceedings of the First International Meeting on High Level Radioactive Waste Management*, Las Vegas, Nevada, April 8-12, 1990. [NNA.900824.0091].
- Brownell, D. H., S. K. Garg, and J. W. Pritchett, "Computer Simulation of Geothermal Reservoirs," Paper SPE 5381, *Proceedings of the 45th California Regional Meeting of the Soc. Pet. Eng. of AIME*, Ventura, California (1975). [NNA.910806.0006].
- Corey, A. T., "The Interrelation Between Gas and Oil Relative Permeabilities," *Prod. Mon.* **19**, 38-41 (1954). [NNA.900720.0036].
- Dalen, V., "Simplified Finite-Element Models for Reservoir Flow Problems," *Soc. Pet. Eng. J.* **19**, 333-343 (1979). [NNA.910806.0007].
- Diaz, J. R., W. R. Jines, and T. Steihaug, "On the Convergence Criterion for Linear (Inner) Iterative Solvers for Reservoir Simulation," Paper SPE 13500 *Proceedings of the Eighth SPE Symposium on Reservoir Simulation*, Dallas, Texas, February (1985). [NNA.890523.0135].
- Gangi, A. F., "Variation of Whole and Fractured Porous Rock Permeability with Confining Pressure," *Rock Mech. Sci. and Geomech. Abstr.* **15**, 249-257 (1978). [NNA.900403.0014].

- Hinton, E., and D. R. J. Owen, *An Introduction to Finite Element Computations* (Pineridge Press, Swansea, Wales, 1979). [NNA.910806.0008].
- Klavetter, E. A., and R. R. Peters, "Estimation of Hydrologic Properties of an Unsaturated Fractured Rock Mass," Sandia Report SAND84-2642, 1986. [HQS.880517.3118].
- Meijerink, J. A., and H. A. Van der Vorst, "An Iterative Solution Method for Linear Systems of Which the Coefficient Matrix is a Symmetric M-Matrix," *Mathematics of Computation* 31, 148-162 (1977). [NNA.890523.0134].
- Mercer, J. W. and C. R. Faust, "Simulation of Water- and Vapor-Dominated Hydrothermal Reservoirs," Paper SPE 5520, *Proceedings of the 50th Annual Fall Meeting of the Soc. Pet. Eng. of AIME*, Dallas, Texas (1975). [NNA.910806.0009].
- Moench, A. F., "Double-Porosity Models for a Fissured Groundwater Reservoir with Fracture Skin," *Water Resources Reference* 20:7, 831-846 (1984). [HQS.880517.2762].
- Molloy, M. W., "Geothermal Reservoir Engineering Code Comparison Project," *Proceedings of the Sixth Workshop on Geothermal Reservoir Engineering*, Stanford University (1980). [NNA.910806.0010].
- Nitao, J., "Numerical Modeling of the Thermal and Hydrological Environment Around a Nuclear Waste Package Using the Equivalent Continuum Approximation: Horizontal Emplacement," Lawrence Livermore National Laboratory report UCID-21444(1988). [NNA.890317.0021].
- Pruess, K., "TOUGH Users Guide," Lawrence Berkeley Laboratory report LBL-20709 (June 1987). [NNA.890315.0010].
- Robinson, B. "Sorption Column Modeling for LiBr," Los Alamos document Group EES-4/7-88-1 (July 1988). [NNA.910806.0011].
- Saad, Y., and M. H. Schultz, "GMRES: A Generalized Minimal Residual Algorithm for Solving Non-Symmetric Linear Systems," *SIAM Journal of Scientific and Statistical Computation* 7(3), 856-869 (1986). [NNA.890523.0137].
- Satter, A., W. M. Shum, W. T. Adams, and L. A. Davis, "Chemical Transport in Porous Media with Dispersion and Rate-Controlled Adsorption," *Soc. Pet. Eng. J.* 20, 129-138, (1980). [NNA.910806.0012].
- Thomas, L. K., and R. G. Pierson, "Three Dimensional Reservoir Simulation," *Soc. Pet. Eng. J.* 18, 151-161 (1978). [NNA.910806.0013].

- Toronyi, R. M., and S. M. Farouq Ali, "Two-phase, Two-dimensional Simulation of a Geothermal Reservoir and Wellbore System," *Soc. Pet. Eng. J.* **17**, 171-183 (1977). [NNA.910806.0014].
- van Genuchten, M. T. "A Closed Form Equation for Predicting Hydraulic Conductivity of Unsaturated Soils," *Soil Sci. Soc. Am. J.*, **44**, 892-898 (1980). [NNA.890522.0287].
- Warren, J. E., and P. J. Root, "The Behavior of Naturally Fractured Reservoirs," *Soc. Pet. Eng. J.* **3**, 245-255 (1963). [NNA.890522.0276].
- Weeks, E. P., "Effect of Topography on Gas Flow in Unsaturated Fractured Rock: Concepts and Observations," *Proceedings of the American Geophysical Union Symposium on Flow and Transport in Unsaturated Fractured Rock*, D. Evans and T. Nicholson, Eds., Geophysical Monograph 42, AGU (1987). [HQS.880517.3217].
- Young, L. C., "A Finite Element Method for Reservoir Simulation," *Soc. Pet. Eng. J.* **21**, 115-128 (1981). [NNA.910806.0015].
- Zienkiewicz, O. C., *The Finite Element Method* (McGraw-Hill, London, 1977). [NNA.910327.0066].
- Zienkiewicz, O. C., and C. J. Parekh, "Transient Field Problems: Two and Three Dimensional Analysis by Isoparametric Finite Elements," *Int. J. Numer. Methods Eng.* **2**, 61-70 (1970). [NNA.910806.0016].
- Zyvoloski, G., "Finite Element Methods for Geothermal Reservoir Simulation," *Int. J. Numer. Anal. Methods Geomech.* **7**, 75-86 (1983). [NNA.910806.0017].
- Zyvoloski, G., "Incomplete Factorization for Finite Elements," *International Journal for Numerical Methods in Engineering* **23**, 1101-1109, 1986. [NNA.890523.0138].
- Zyvoloski, G. and Z. Dash, "Software Verification Report FEHMN Version 1.0," Los Alamos National Laboratory report LA-UR-91-609 (1991). [NNA.910806.0018].
- Zyvoloski, G., Z. Dash, and S. Kelkar, "FEHM: Finite Element Heat and Mass Transfer Code," Los Alamos National Laboratory report LA-11224-MS (March 1988). [NNA.900918.0013].





**The following number is for Office of Civilian Radioactive Waste Management (OCRWM) records management purposes only and should not be used when ordering this publication.**

**Accession Number NNA.910625.0038**

**This report has been reproduced directly from the best available copy.**

**It is available to DOE and DOE contractors from the Office of Scientific and Technical Information, P.O. Box 62, Oak Ridge, TN 37831. Prices are available from (615) 576-8401, FTS 626-8401.**

**It is available to the public from the National Technical Information Service, U.S. Department of Commerce, 5285 Port Royal Rd., Springfield, VA 22161.**

