## Enclosure 2 PG&E Letter DCL-99-030

## Calculation Notebook STA-042

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MADE BY_	<u>H M Lee</u> DATE	<u>10/1/96</u> CHECK	BY L R Chang	APPROVED_BY

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1. Introduction

The inspection of steam generator tubes has identified tube cracks in the portions of tubes surrounded by the tube support plats. Since the tube support plats hold up the tubes, the tubes will not be burst even if cracks have been developed on the tube wall in these regions. Therefore, plugging these tubes may not be required. However, a concern was raised during steam line break accident. The fast pressure transient in the steam generator during steam line break accident may result in high pressure load on the tube support plats which may push the tube support plats up from their original locations. The concern is that, if the tube support plats are pushed up during the steam line break. the tube cracks in these regions will not be protected by the tube support plats and will be exposed to the high pressure difference from the primary side to the secondary side *ord* fail.

The purpose of this calculation is to calculate the pressure loads on the tube support plats during the steam line break accident. The RELAP5 code mod 3.2 is used to perform the calculation. The results of this calculation then be transferred to Westinghouse to perform structure analysis to determine the displacement of the tube support plats. Since the larger the break size results in the higher pressure load on the tube support plats, the break at the steam generator steam outlet nozzle is used. In addition, the break at the downstream of the main steam flow

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restrictor is also analyzed.

The initial plant condition is assumed to be hot 0% power. The study of the conservatism for the initial plant condition assumption is not part of the scope of this calculation. Westinghouse already modeled the steam generator (Westinghouse Model 51) at hot 0% power using the TRANFLO code for Farley Plant (ref. 1). The Farley Model 51 steam generators are identical to the DCPP Model 51 steam generators, except for the wrapper opening at the tube sheet (Ref. 2). Therefore, in this calculation, the TRANFLO model for the steam generator is used as the bases for setting up the RELAP5 steam generator model.

Assumptions 2.

The following assumptions are used in this calculation.

- The plant is at hot 0% power. 1.
- The steam line break is located at the steam generator steam outlet 2. nozzle which is upstream of the steam flow restrictor and has the largest steam flow area. The break at the downstream of the flow restrictor is also analyzed.
- Since the high pressure loads on the tube support plats only last 3. for less than 2 seconds, the heat transfer from the RCS to the steam generator secondary side does not have significant effect on the

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pressure load on TSPs. The primary coolant flow is assumed at constant flow rate of 9148.5 lb/sec and the primary coolant pressure and temperature specified in Ref. 1 are used.

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- 4. The steam line break induces tremendous high steam and water flow in the steam generator and the high pressure loads on the tube support plats only last for less than 2 seconds. The initial flow in the steam generator secondary side and the auxiliary feedwater injected into the steam generator have insignificant effects on the fast transient occurred in the steam generator. It is assumed that no steam is removed from the steam generator before the break and the auxiliary feedwater flow is not included in the steam generator model. The RELAP5 model does not assign any flow to the junctions of the steam generator secondary side. However, a five seconds steady state run is performed before the break is initiated which generates a natural recirculate flow in the secondary side of the steam generator due to the heat transferred from the primary side.
- 5. The RELAP5 code manual (Ref. 3) recommends to use the nonequilibrium model for all volumes. However, the use of nonequilibrium model for the shell side of the tube region generates more abrupt changes in the pressure loads which do not show with the use of equilibrium model for the shell side of the tube region. Since it is difficult to determine which model will generate more conservative loads on the TSPs, the non-equilibrium and equilibrium

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models are used to model the shell side of the tube region in separated cases to calculate the loads on TSPs.

 The roughness for commercial steel pipe is 0.00015 ft (or 0.0018") (Ref.) which is used for all volumes.

3. RELAP5/MOD3.2 Code

The RELAP5 code is an advanced-thermal hydraulic code which has been used as a tool to analyze transient in light water reactor systems. The RELAP5/MOD3 code is the third major variant of the RELAP5 code and the RELAP5/MOD3.2 code is the latest revision of the RELAP5/MOD3 code. The RELAP5/MOD3.2 code has been used by analysts to evaluate the thermalrestor hydraulic behavior of many light water systems.

The RELAP5/MOD3.2 code equation set gives a two-fluid system simulation using a non-equilibrium, non-homogeneous, six-equation representation. The six basic field equations are used to solve six dependent variablespressure, specific internal energies for gas and liquid, void fraction and velocities for gas and liquid. Constitutive models represent the interphase drag, the various flow regimes in vertical and horizontal flow, wall friction, and interphase mass transfer. The code also has the capability to simulate the presence of slabs of material adjacent to the

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fluid. Thus, energy transfer to and from stationary slabs of material can be simulated. Control systems and component models permit simulations of equipment controllers, balance-of-plant equipment, and lumped-node representations of various processes.

4. Analysis

There are five cases analyzed in this calculation. These cases are described as follows.

LB Case 1: The plant is at hot 0% power. A steam line break is occurred at the steam generator outlet nozzle. The initial water level in the steam generator is at 490.4 inches from the top  $f_{c}$   $\frac{10/2}{9}$ of the tube plat which is equivalent to narrow range of  $33\frac{6}{5}$ .  $\frac{14m}{11/96}$ The non-equilibrium model is used to model the secondary side of the tube region.

LB Case 2: This case is same as the LB Case 1, except the equilibrium model is s and s model the secondary side of the tube region.

LB Case 3: This case is designed to study the effects of the initial water level and the resistances of the tube support plates on the calculated loads on the TSPs. The lower the initial water level and the higher the TSP resistance result in higher loads on the TSPs. Therefore, for this case, the

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initial water level is the steam generator is reduced to  $466.0^{\circ}$ , which is corresponding to narrow range water level of 16%, 14-176 and the TSP resistance coefficient is increased to 0.99. The remaining conditions for this case are same as those used for LB Case 1.

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- SB Case 1: This case is same as the LB Case 1, except the break is assumed located at the downstream of the main steam flow restrictor.
- SB Case 2: This case is same as the LB Case 2, except the break is assumed located at the downstream of the main steam flow restrictor.

#### 5. RELAP5 Input

The fluid region in the steam generator is separated in two loops. The first loop is the primary loop which models the primary side of the tubes. The second loop is the secondary loop which models the secondary side of the steam generator. Heat slabs are used to model the heat transfer from the primary side to the secondary side.

<u>RELAP5 Model for Steam Generator Secondary Side (Secondary Loop)</u> The schematic diagram for the RELAP5 model for the steam generator

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secondary side is given in Figure 5-1. The RELAP5 model consists of the following elements.

- 2 pipe components Component 2 consists of 30 volumes and 29 junctions. The schematic diagram for the Component 2 is shown in figure 5-2. Component 35 consists of 3 volumes and 2 junctions.
- 2 separator components Component 19 consists of 1 volumes and 3 junctions. Component 22 consists of 1 volumes and 3 junctions.
  5 branch components Component 21 consists of 1 volume and 2 junctions. Component 30 consists of 1 volume and 2 junctions.
  Component 33 consists of 1 volume and 2 junctions. Component 34 consists of 1 volume and 1 junctions. Component 53 consists of 1 volume and 2 junctions.
  - 7 single volume components Components 17, 18, 20, 23, 32, 36 and 38.
- 2 single junction components Components 519 and 533.
- . 1 valve component Component 518.

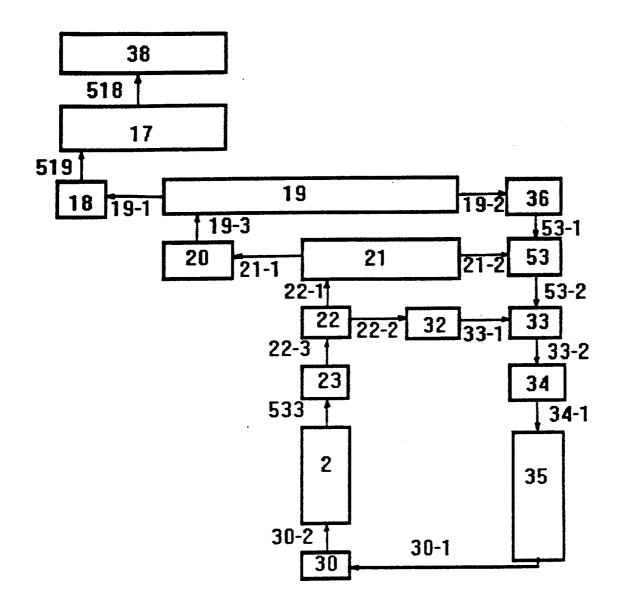
## RELAP5 Model for Steam Generator Primary Side (Primary Loop)

The schematic diagram for the RELAP5 model for the steam generator primary side is given in Figure 5-3. The RELAP5 model consists of the following elements.

. 1 pipe component - Component 1 consists of 60 volumes and 59 junctions.

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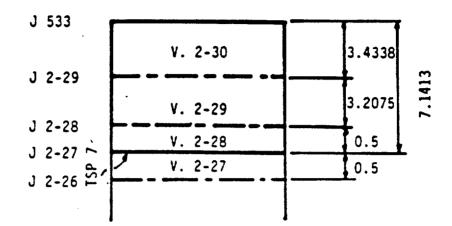


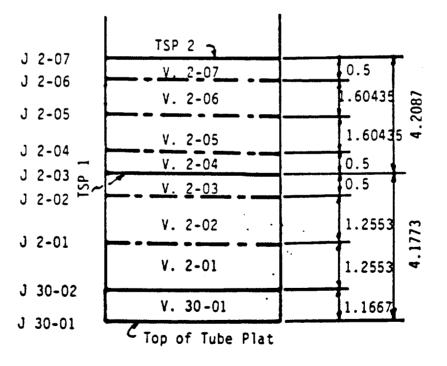
## **RELAP5 Steam Generator Secondary Side Model**

FIGURE 5 - 1

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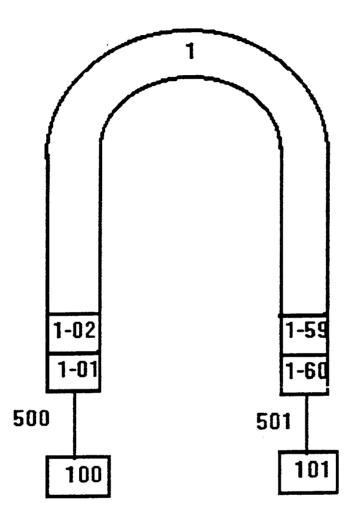
V. = Volume

J = Junction

Component 2 and Component 30

FIGURE 5 - 2

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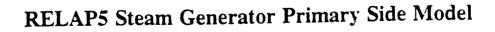


FIGURE 5 - 3

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- . 2 time dependent volume components Components 100 and 101.
- . 2 time dependent junction components Components 500 and 501.

#### Heat Slab

There are 60 heat slabs used to model the tubes and the heat transfer from the primary side fluid to the secondary fluid. Each heat slab connects a primary side volume to a secondary side volume.

#### Common Input

The common RELAP5 input used for the volumes and junctions are listed in this section. The RELAP5/MOD 3.2 code has certain options available for modeling the volumes and junctions which can be switched on or off by the volume control flags and junction control flags. Since the steam line break transient is a very short and fast transient with huge flows in the secondary side of the steam generator, the defaulted options are selected to model the volumes and junctions, except specially discussed and specified for particular volumes or junctions. The switching from nonequilibrium volume model to equilibrium volume model to model the shell side of the tube region has significant effects on the TSPs' loads. As described in Section 4, a sensitivity study is performed to study the effects of switching from the non-equilibrium to the equilibrium volume model for the volumes modeling the shell side of the tube region.

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The RELAP5/MOD3.2 options for modeling the volumes and junctions associated with the defaulted volume control flags and junction control flags are listed as follows.

Volume Control Flags

- . t=0, the thermal front tracking model is not used.
- . 1=0, the mixture level tracking model is not used.
- . p=0, the water packing scheme is used.
- . v=0, the vertical stratification model is used.
- . b=0, the pipe interphase friction model is used.
- . f=0, the wall friction is used.
- . e=0, the non-equilibrium model is used.

Junction Control Flags

- . e=0, the modified PV term is not used.
- . f=0, the CCFL model is not used.
- . v=0, the horizontal stratification entrainment model is not used.
- . c=0, the chocking model is used.
- . a=0, a smooth area change or no area change.
- . h=0, the non-homogeneous model is used.
- . s=0, the momentum fluxes to the volume and from the volume are used.

As described in Section 2, the roughness of 0.00015 ft is used for all

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the Volumes and the initial liquid and vapor mass flow rates are zero for all the junctions which will not be discussed again for each Component. The description of the input variables is given in the Reference 4.

The default input value is used for all the input data which are not described in this section.

#### RELAP5 Input for LB Case 1

The Initial conditions for LB Case 1 are same as those specified in Reference 1 for the case with the steam generator water level 490.5" from the top of the tube plat and hot 0% power.

#### Secondary Loop

The secondary loop includes 16 components - 2, 17, 18, 19, 20, 21, 22, 23, 30, 32, 33, 34, 35, 36, 38, 53, 518, 519 and 533. A schematic of the secondary loop is shown in the Figure 5-1.

#### Component 30

Component 30 is a Branch with assigned component name "tubesh" which includes a single volume (30-01) and two junctions (30-01 and 30-02). The Volume 30-01 models the shell side of the tube region from the top of (Ref. 1) the tube plat to the height of the wrapper opening which is 14". The Junction 30-01 is from the downcomer (Component 35) to the Component 30

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and the Junction 30-02 is from the Component 30 to the remaining shell side of the tube region (Component 2).

As given in Ref. 1, the flow area of the shell side of tube region is 54.22 ft<sup>2</sup>. The length for the Volume 30-01 is 14" or 1.1667'. Since the Volume 30-01 is orientated as 90 degree upward, the elevation change for the Volume 30-01 is 1.1667'. The hydraulic diameter of 0.136' is used in the TRANFLO model for the shell side of tube region (Ref. 1). The same hydraulic diameter is used for the Volume 30-01. Since the Volume 30-01 contains rod bundle, the volume control flag b is set to be 1 which initiates the use of the rod bundle interphase friction model.

As used in the TRANFLO model (Ref. 1), the water temperature of the steam generator secondary side is 547 °F. The specific volume for water at 547 °F is 0.02166 ft<sup>3</sup>/lb. The water density at 547 °F is 46.17 lb/ft<sup>3</sup>. The pressure at the center of node 31 of TRANFLO model is 1033.66 psia which is located 4.21/2 = 2.105 ft from the top of the tube plat. The pressure at the center of the volume 30-01 can calculated as: 1033.66 + (2.105 - 1.1667/2) \* 46.17 / 144 = 1034.15 psia

The flow area of Junction 30-01 is same as the flow area of Component 35 which is 7.096 ft<sup>2</sup>. The forward and reverse flow resistant coefficients for Junction 30-01 should be same as those given for the segment 1 of the

Connector 30 or 31 which are 0.5 and 0.5.

The flow area of Junction 30-02 equals to the cross section flow area of the wrapper opening in the horizontal direction which was calculated as 2.215 ft<sup>2</sup> for the Farley Model 51 steam generator (combining the flow area given in the TRANFLO model for the Connector 30 segment 2 and the Connector 31 segment 2). The wrapper opening height for Farley steam DCPP's generator is 7" (Ref. 2), while the wrapper opening height is 14". Therefore, the flow area of Junction 30-02 is 2.215 \* 2 = 4.43 ft<sup>2</sup>. As given in Westinghouse letter NSD-JLH-6070, the flow resistant coefficient for the cross flow through the wrapper opening is 5.32 based on flow area of 4.43 ft<sup>2</sup>. The Westinghouse letter is attached to this calculation as Appendix A. Therefore, the forward and reverse flow resistant coefficients of 5.32 are used for the Junction 30-02. The following input are specified for the Component 30. branch 0300000 tubesh 1 0300001 2 90. 1.1667 0.00015 0.136 00100 1,1667 0, 0, 54.22 0300101 0300200 1034.15 547.0 3 0.5 000000 7.096 0.5 035010000 030000000 0301101

0302101 030010000 002000000 4.43 5.32 5.32 000000

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#### Component 2

The Component 2 is a Pipe with assigned name shell which is used to model the secondary side from the top of wrapper opening to the bottom of the primary separator. There are 30 volumes and 29 junctions included in the Component 2. The modeling scheme of the Component 2 is shown in the Figure 5-2. Volumes 2-01 to 02-03 are used to model the region from the top of the wrapper opening to the middle of the TSP 1. Volumes 2-04 to 02-07 are used to model the region from the middle of the TSP 1 to the middle of TSP 2. Volumes 2-08 to 2-11 are used to model the region from the middle of TSP 2 to the middle of the TSP 3. Volumes 2-12 to 2-15 are used to model the region from the middle of TSP 3 to the middle of the TSP 4. Volumes 2-16 to 2-19 are used to model the region from the middle of TSP 4 to the middle of the TSP 5. Volumes 2-20 to 2-23 are used to model the region from the middle of TSP 5 to the middle of the TSP 6. Volumes 2-24 to 2-27 are used to model the region from the middle of TSP 6 to the middle of the TSP 7. Volumes 2-28 to 2-30 are used to model the region from the middle of TSP 7 to the bottom of the primary separator.

To calculate the pressure difference across the TSP, a volume length of 0.5 ft is used for all the volumes adjacent to the TSP (volumes 2-03, 2-04, 2-07, 2-08, 2-11, 2-12, 2-15, 2-16, 2-19, 2-20, 2-23, 2-24, 2-27, 2-

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 Image: Constraint on the Steam Generator Support Plats During SLB Accident

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The length between the TSPs not including the thickness of the TSP 28). is given in the TRANFLO model as  $2.073 \times 2 = 4.146$  ft (the sum of the length of segments 1 and 3 of the Connectors 40). The thickness of the TSP is given in the TRANFLO model as 0.0625 ft (the length of the segment 2). The length between the middle of TSPs is 4.146 + 0.0625 = 4.2085 ft (4.2087 ft is used in this calculation, the effect is insignificant). The length from the top of tube plat to the middle of TSP 1 is 1.146 + 0.0625/2 = 4.1773 ft. To makeup the 4.1773 ft, the volume length for 0.0625/2 = 4.1773 ft. To makeup the 4.1773 ft, the volume length for 144/4/4volume 2-01 and 2-02 is (4.1773 - 1.1667 (length of Volume 30-01) - 0.5)/2.  $f_{c} \frac{1}{2} \frac{1}{2} \frac{1}{2}$ = 1.2553 ft. The volume length for the volumes between the TSPs but not adjacent to the TSPs (Volumes 2-05, 2-06, 2-09, 2-10, 2-13, 2-14, 2-17, 2-18, 2-21, 2-22, 2-25 and 2-26) can be calculated as (4.2087 - 0.5 -0.5)/2 = 1.60435 ft. As given in the TRANFLO model (Ref. 1), the length from the top of the TSP 7 to the bottom of the primary separator is 7.11 ft (length of Node 24). Including the half of the TSP thickness, the sum of the volume length for Volume of 2-28, 2-29 and 2-30 should be 7.11 + 0.0625/2 = 7.1413 ft (see Figure 5-2). As given in the TRANFLO model (Ref. 1), the average length for the tube above the TSP 7 is 44.49" or 3.7075' (length for the Nodes 9 and 8). The Volume 2-28 and 2-29 are used to model the region with tubes and the Volume 2-30 does not have tube inside. Therefore, the volume length for Volume can be determined as 3.7075 - 0.5 =3.2075 ft. The volume length for Volume equals to 7.1413 - 0.5 - 3.2075 = 3.4338 ft.

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The flow areas for the Volumes 2-01 to 2-27 are the same as the flow areas used for the TRANFLO Nodes 31 to 25 which are 54.22 ft<sup>2</sup>. The flow areas for the Volumes 2-28 to 2-30 are the same as the flow areas for the TRANFLO Nodes 24 which is 70.0 ft<sup>2</sup>. The flow areas for the Junctions of Component 2 are the same as the flow areas for the adjacent Volumes, except the flow areas for the Junctions modeling the TSPs. The flow areas for the TSPs are given in the TRANFLO model (Ref. 1) as 23.716  $ft^2$ . Therefore, the flow area of 54.22  $ft^2$  is used for the Junctions 2-01, 2-02, 2-04, 2-05, 2-06, 2-08, 2-09, 2-10, 2-12, 2-13, 2-14, 2-16, 2-17, 2-18, 2-20, 2-21, 2-22, 2-24, 2-25 and 2-26. The flow area for 23.716 ft<sup>2</sup> is used for the Junctions 2-3, 2-7, 2-11, 2-15, 2-19, 2-23 and 2-27. The flow area of 70  $ft^2$  is used for the Junctions 2-28 and 2-29.

The volume sizes for all the Volumes are not specified by the input (0.0 is input for volume side). The RELAP5 code will calculate the volume size based on the volume flow area and length. All the Volumes of Component 2 are vertical upward volumes. A 90° inclination angle is used for all the volumes. For all the Volumes, the elevation changes are the same as the volumes lengths. As the Volume 30-01, the hydraulic diameter 0.136 of  $\rho_{216}$  ft is used for all the Volumes, except the volume 2-30 (no tubes in the Volume 2-30). For the Volume 2-30, the hydraulic diameter is calculated by the RELAP5 code.

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Same as the Volume 30-01, since rod bundle is contained in the Volumes 2-01 to 2-29, the volume control flag b is set to be 1 for Volumes 2-01 to 2-29 which initiates the use of the rod bundle interphase friction model.

The initial water temperature for all the volume of Component 2 is 547 °F. As calculated for Volume 30-01, the water density is  $46.17 \text{ lb/ft}^3$ . The water static pressure reduces 46.17/144 = 0.3206 psi for every foot elevation increase. The initial pressure for Volume 30-01 is 1034.15 psia. The initial pressure used in TRANFLO model for Node 24 is 1023.75 psia (Ref. 1). The elevation at the center of the Node 24 is 7.11/2 =3.555 ft below the bottom of the primary separator. The elevation at the center of the Volume 2-30 is 3.4338 /2 =1.7169 ft below the bottom of the primary separator. The initial pressure at the center of the Volume 2-30 should be 1023.75 - (3.555 - 1.7169) \* 0.3206 = 1023.17 psia. The pressure for the remaining Volumes of Component 2 can calculated by elevation difference from the Volume 2-30. Since a 5 seconds steady state run is performed to straighten out slight inconsistence of the initial conditions, high accuracy for the initial pressure input for the Volumes of Components 2 is not required. The initial pressures for the Volumes of Component 2 are calculated as follows. 1023.17 + (3.2075 +3.4338)/2\*0.3206 = 1024.23 psia. Volume 2-29 1024.23 + (3.2075 +0.5)/2\*0.3206 = 1024.82 psia. Volume 2-28

Volume 2-27 1024.82 + (0.5 + 0.5)/2\*0.3206 = 1024.98 psia.

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Volume 2	-26	1024.98	÷	(0.5 + 1.60435)/2*0.3206 = 1025.32 psia.
Volume 2	-25	1025.32	+	(1.60435+1.60435)/2*0.3206 = 1025.83 psia.
Volume 2	-24	1025.83	÷	(1.60435+0.5)/2*0.3206 = 1026.17 psia.
Volume 2	-23	1026.17	+	(0.5 +0.5)/2*0.3206 = 1026.32 psia.
Volume 2	-22	1026.32	+	(0.5 +1.60435)/2*0.3206 = 1026.66 psia.
Volume 2	-21	1026.66	+	(1.60435+1.60435)/2*0.3206 = 1027.18 psia.
Volume 2	-20	1027.18	+	(1.60435+0.5)/2*0.3206 = 1027.52 psia.
Volume 2	-19	1027.52	+	(0.5 +0.5)/2*0.3206 = 1027.68 psia.
Volume 2	-18	1027.68	+	(0.5+1.60435)/2*0.3206 = 1028.01 psia.
Volume 2	2-17	1028.01	+	(1.60435+1.60435)/2*0.3206 = 1028.53 psia.
Volume 2	2-16	1028.53	+	(1.60435+0.5)/2*0.3206 = 1028.86 psia.
Volume 2	2-15	1028.86	+	(0.5+0.5)/2*0.3206 = 1029.02 psia.
Volume 2	2-14	1029.02	+	(0.5+1.60435)/2*0.3206 = 1029.36 psia.
Volume 2	2-13	1029.36	+	(1.60435+1.60435)/2*0.3206 = 1029.87 psia.
Volume 2	2-12	1029.87	+	(1.60435+0.5)/2*0.3206 = 1030.21 psia.
Volume 2	2-11	1030.21	÷	(0.5+0.5)/2*0.3206 = 1030.37 psia.
Volume 2	2-10	1030.37	+	(0.5+1.60435)/2*0.3206 = 1030.71 psia.
Volume 2	2-09	1030.71	+	(1.60435+1.60435)/2*0.3206 = 1031.22 psia.
Volume 2	2-08	1031.22	+	(1.60435+0.5)/2*0.3206 = 1031.56 psia.
Volume 2	2-07	1031.56	+	(0.5+0.5)/2*0.3206 = 1031.72 psia.
Volume 2	2-06	1031.72	÷	(0.5+1.60435)/2*0.3206 = 1032.06 psia.
Volume á	2-05	1032.06	+	(1.60435+1.60435)/2*0.3206 = 1032.57 psia.
Volume 2	2-04	1032.57	+	(1.60435+0.5)/2*0.3206 = 1032.91 psia.

SUBJECT	Loads on '	the Steam	Generator	Support	<u>Plats</u>	During SLE	<u>Accident</u>
MADE BY_	H M Lee D	ATE <u>10/1</u>	<u>796</u> CHECK	BY L R	Chang	APPROVED	BY

1032.91 + (0.5+0.5)/2\*0.3206 = 1033.07 psia Volume 2-03 1033.07 + (0.5+1.2553)/2\*0.3206 = 1033.35 psia Volume 2-02 1033.35 + (1.2553+1.2553)/2\*0.3206 = 1033.73 psia Volume 2-01 The hydraulic diameter is used in the CCFL correction and the interphase drag. As shown on the input for the segment 2 of connectors 34 to 40 of the TRANFLO model, the hydraulic diameter of 0.0625 ft is used for the TSPs and the resistance coefficient of 0.78 is used for both forward and reverse flow through the TSPs which includes the resistance due to area change at the TSPs. The CCFL correlation is not used in this calculation. All the junctions of the Component 2 except those associated with TSPs have no resistance. The default values for all the CCFL data are used for all junction of the Component 2. The following input are used for the Component 2.

0020000 shell pipe

0020101	54.22	27
0020102	70.0	30
0020201	54.22	2
0020202	23.716	3
0020203	54.22	6
0020204	23.716	7
0020205	54.22	10
0020206	23.716	11

## SHEET NO. 23 OF/74 SHEETS CALC NO. STA-042 R.O

SUBJECT	Loads on t	he Steam Generat	or Support Plats	During SLB Accident
MADE BY	HM 185	DATE 10/1/96 CH	IECK BY	APPROVED BY

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0020207	54.22	14
0020208	23.716	15
0020209	54.22	18
0020210	23.716	19
0020211	54.22	22
0020212	23.716	23
0020213	54.22	26
0020214	23.716	27
0020215	70.0	29
0020301	1.2553	1
0020302	1.2553	2
0020303	0.5	4
0020304	1.60435	6
0020305	0.5	8
0020306	1.60435	10
0020307	0.5	12
0020308	1.60435	14
0020309	0.5	16
0020310	1.60435	18
0020311	0.5	20
0020312	1.60435	22
0020313	0.5	24
0020314	1.60435	26

## SHEET NO. 2 POF/79 SHEETS CALC NO. STA-042 RO

SUBJECT	Loads on the S	team Generator Suppor	t Plats During SLB Accident	
MADE BY	HALEG DATE	/0/1/96 CHECK BY	APPROVED BY	
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0020315	0.5	28		
0020316	3.2075	5 29		
0020317	3.4338	3 30		
0020601	90.0	30		
0020801	0.000]	15 0.1	36	29
0020802	0.000]	15 0.0		30
<b>002</b> 0901	0.0	0.0	2	
0020902	0.78	0.78	3	
0020903	0.0	0.0	6	
0020904	0.78	0.78	7	
0020905	0.0	0.0	10	
0020906	0.78	0.78	11	
0020907	0.0	0.0	14	
0020908	0.78	0.78	15	
0020909	0.0	0.0	18	
0020910	0.78	0.78	19	
0020911	0.0	0.0	22	
0020912	0.78	0.78	23	
0020913	0.0	0.0	26	
0020914	0.78	0.78	27	
0020915	0.0	0.0	29	
0021001	00100	29		
0021002	00000	30		

#### PACIFIC GAS AND ELECTRIC COMPANY COMPUTATION SHEETSHEET NO.25 OF/76 SHEETS<br/>CALC NO. STA-092 ROLoads on the Steam Generator Support Plats During SLB AccidentHM LTG DATE 10/1/92 CHECK BY GENERAL COMPUTATION SHEET SUBJECT MADE BY HAN LEG DATE 10/1/96 CHECK BY 29 000000 0021101 1 0.0 0.0 547.0 0.0 1033.73 0021201 3 0.0 2 547.0 0.0 0.0 1033.34 0021202 3 0.0 3 0.0 0.0 1033.07 547.0 0021203 3 0.0 4 0.0 0.0 547.0 1032.91 0021204 3 5 0.0 0.0 547.0 0.0 1032.57 0021205 3 0.0 0.0 6 1032.06 547.0 0.0 0021206 3 7 0.0 0.0 0.0 1031.72 547.0 3 0021207 0.0 8 0.0 1031.56 547.0 0.0 0021208 3 9 0.0 547.0 0.0 0.0 1031.22 3 0021209 10 -0.0 0.0 547.0 0.0 1030.71 0021210 3 0.0 11 1030.37 547.0 0.0 0.0 3 0021211 0.0 0.0 12 547.0 0.0 1030.21 0021212 3 0.0 0.0 13 0.0 1029.87 547.0 0021213 3 0.0 0.0 0.0 14 547.0 1029.36 0021214 3 0.0 0.0 15 0.0 547.0 0021215 3 1029.02 16 0.0 0.0 0.0 1028.86 547.0 0021216 3 0.0 17 0.0 1028.53 547.0 0.0 3 0021217 18 0.0 0.0 1028.01 547.0 0.0 3 0021218

0.0

0.0

0.0

0.0

547.0

547.0

547.0

547.0

3

3

3

3

0021219

0021220

0021221

0021222

1027.68

1027.52

1027.18

1026.66

0.0

0.0

0.0

0.0

0.0

0.0

0.0

0.0

19

20

21

22

PACIFIC GAS GENERAL COMP	UTATIO	N SHEET	SHEET NO. 26 OF 174 SHEETS CALC NO. STA- 062 R.O				
SUBJECT Lo	ads on	the Stear	n Generat	tor Sup	oport_	<u>Plats</u>	During SLB Accident
	1156	DATE/o	1/96 CI	HECK B	Y		APPROVED BY
0021223	3	1026.33	547.0	0.0	0.0	0.0	23
0021224	3	1026.17	547.0	0.0	0.0	0.0	24
0021225	3	1025.83	547.0	0.0	0.0	0.0	25
0021226	3	1025.32	547.0	0.0	0.0	0.0	26
0021227	3	1024.98	547.0	0.0	0.0	0.0	27
0021228	3	1024.82	547.0	0.0	0.0	0.0	28
0021229	3	1024.23	547.0	0.0	0.0	0.0	29
<b>002</b> 1230	3	1023.17	547.0	0.0	0.0	0.0	30

29

1.0

29

0.0

1.0

#### Component 533

0021300

0021301

0021401

1

0.0

0.0625

0.0

0.0

The Component 533 is a single junction with assigned name abovetb which is used to provide a flow junction from the Volume 02-30 (Component 2) to the Volume 23-01 (Component 23). This component consists of 1 junction (Junction 533). The Junction 533 is corresponding the Connector 33 of the TRANFLO model given in Reference 1.

The smaller of the two flow areas of Volumes 2-30 and 23-01 is 49.43  $ft^2$ which is used as the flow area for this junction. As given the Reference 1, no flow resistance coefficient is specified for the Connector 33 while

CALC NO.

SUBJECT	loads on	the Steam Gen	erator Support	Plats During SLB Accident
MADE BY	1th LEE	DATE 10/1/96	_CHECK BY	APPROVED BY

the abrupt flow area change is specified for the Connector 33. The forward and reverse flow resistant coefficient of 0.0 is used for this junction. The junction control flag a is set to 1 to specify an abrupt area change. The following input are used for the Component 533. abovertb snqljun 5330000 49.43 0.0 0.0 000100 023000000 002010000 5330101 5330110 0.0 0.0 1.0 1.0 0.0 0.0 0.0 5330201 1

#### Component 23

The Component 23 is a single volume with assigned name abovetb which is used to model the region inside the primary separator and below the swirl vane. This component consists of 1 volume (Volume 23-01). The Volume 23-01 is corresponding the Node 23 of the TRANFLO model given in Reference 1. As given in the Table 4.2.2 of Reference 1, the flow area and volume size for the Node 23 are 49.43  $ft^2$  and 244.3  $ft^3$ . The volume length of Node 23 is 244.3/49.43 = 4.9423 ft. The flow area and volume length are specified as input data while the volume size is not specified which will be calculated by the code using the volume length and flow area.

The Volume 23 is a vertical upward volume. The inclination angle is  $90^\circ$ and the elevation change is same as the volume length. The hydraulic

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diameter of the volume is not specified also and the code will calculate it.

The initial water properties for Node 23 are given in Reference 1 as water pressure at 1022.72 psia, water temperature at 547°F and void  $MC^{1/176}$  fraction of 0.03. The RELAP5/MOD3.2 code recognizes the water quality for  $V^{1/16}$ AL 1/1/96 instead of void fraction. The void fraction and water quality are identical when the water is in pure liquid phase (void fraction and quality are zero) and the water is pure vapor phase (void fraction and There are 5 components (23, 32, 33, 53 and 36) having quality are one). water in two phases initially. The void fractions specified in the TRANFLO model for the corresponding nodes are used for these 5 components. This results in higher void fractions in these components which is equivalent to reduce the initial water level. In Reference 1. a sensitivity study using TRANFLO code was performed which concluded that the lower the initial water level generates higher loads on the TSPs. A sensitivity study is also performed using RELAP5 code to verify this conclusion. The sensitivity study is attached in the Appendix B. For all the five cases discussed in Section 4, the void fractions given in the TRANFLO model are used as water qualities in RELAP5 analysis.

For two phases fluid, the RELAP5 code does not allow to specify both the water pressure and temperature. The water pressure of TRANFLO Node 23 is

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 SUBJECT
 Loads on the Steam Generator Support Plats During SLB Accident

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used for this component. The initial water properties are specified as
pressure at 1022.72 psia and the quality of 0.03. The following input
are used for Component 23.
0230000 abovetb snglvol
0230101 49.43 4.9423 0.0 0.0 90.0 4.9423 0.00015 0.0 00000
0230200 2 1022.72 0.03

#### Component 22

The Component 22 is a separator with assigned name speratr which is used to model the region inside the primary separator and above the swirl fan. This component consists of 1 volume (Volume 22-01) and 3 junctions (Junctions 22-01, 22-02 and 22-03). The Volume 22-01 is corresponding the Node 22 of the TRANFLO model given in Reference 1. As given in the Table 4.2.2 of Reference 1, the flow are and volume size for the Node 22 are 41.73 ft<sup>2</sup> and 163.4 ft<sup>3</sup>. The volume length of Node 22 is 163.4/41.73 = 3.9156 ft. The flow area and volume length are specified as input data while the volume size is not specified which will be calculated by the code using the volume length and flow area.

The Volume 22-01 is a vertical upward volume. The inclination angle is 90° and the elevation change is same as the volume length. The hydraulic diameter of the volume is not specified also and the code will calculate it.

 GENERAL COMPUTATION SHEET
 CALC NO. STA-DUL R.D

 SUBJECT
 Loads on the Steam Generator Support Plats During SLB Accident

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SHEET NO. 30 OF/74 SHEETS

The initial water properties for Node 22 are given in Reference 1 as pressure at 1021.14 psia, temperature at 547°F and void fraction of 1.0 (pure steam). Since there is no superheated steam in the steam generator, the steam in volume 22-01 must be saturated steam. For saturated steam, the RELAP5 code does not allow to specify both the water pressure and temperature. The steam pressure of TRANFLO Node 22 is used for this component. The initial water properties are specified as pressure at 1021.14 psia and the quality of 1.0.

The Junction 22-01 connects the outlet of Volume 22-01 to the inlet of Volume 21-01 which is corresponding to the Connector 26 of the TRANFLO model. As given in the Reference 1, the smallest flow area of the three segments of the Connector 26 is 12.828 ft<sup>2</sup> and a forward and reverse flow resistant coefficients of 0.84 and 0.47 are associated with this flow area.

The Junction 22-02 connects the inlet of Volume 22-01 to the inlet of Volume 32-01 which is corresponding to the Connector 27 of the TRANFLO model. The smaller of the two flow areas of Volumes 22-01 and 32-01 is 17.35 ft<sup>2</sup> which is used as the flow area for this junction. As given the Reference 1, flow resistance is specified for the segments 2 and 3 of the Connector 27, a forward and reverse flow resistant coefficient of 0.5 associated with a flow area of 30.579 ft<sup>2</sup> for segment 2 and a forward and

		CALC NO. STA- 042 R.O
SUBJECT	Loads on the Steam Generator Support	Plats During SLB Accident
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SHEET NO.3/ OF/74 SHEETS

reverse flow resistant coefficient of 0.5 associated with a flow area of 18.579 ft<sup>2</sup> for segment 3. Therefore, for Junction 22-02, the flow resistant coefficient associated with the flow area of 17.35 ft<sup>2</sup> can be calculated as:

 $0.5/(30.579/17.35)^2 + 0.5/(18.579/17.35)^2 = 0.161 + 0.436 = 0.597$ 

The Junction 22-03 connects the outlet of Volume 23-01 to the inlet of Volume 22-01 which is corresponding to the Connector 32 of the TRANFLO model. The smaller of the two flow areas of Volumes 23-01 and 22-01 is 41.73 ft<sup>2</sup> which is used as the flow area for this junction. As given the Reference 1, a forward and reverse flow resistant coefficient of 10.0 associated with a flow area of 44.768 ft<sup>2</sup> is specified for the segment 2 of the Connector 32. Therefore, for Junction 22-03, the flow resistant coefficient associated with the flow area of 41.73 ft<sup>2</sup> can be calculated as:

 $10.0/(44.768/41.73)^2 = 8.689$ 

The following input are used for the Component 22. 0220000 speratr separatr 0220001 1 3 3.9156 0.0 0. 90. 3.9156 0.00015 00000 0.0 0220101 41.73 1021.14 1.0 0220200 2 000000 022010000 021000000 12.828 0.84 0.47 0221101

SHEET NO. 32 OF/ 74 SHEETS CALC NO. STA- 842 R.O

SUBJECT	loads on the Steam	Generator Support	Plats During SLB Accident
MADE BY	IM LEG DATE 10/1	196 CHECK BY	APPROVED BY
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0222101	02200	0000	032000000	17.35	0.597	0.597	000000	
<b>0223101</b>	02301	0000	022000000	41.73	8.689	8.689	000000	
0221201	0.0	0.0	0.0					
0222201	0.0	0.0	0.0					
0223201	0.0	0.0	0.0					

#### Component 21

1+1 ( 10/1/96 fe 10/2/96

1+11 10/1/96

HAC 10/1196

fe 192/96

The Component 21 is a branch with assigned name abovspr which is used to model the region below the secondary separator and above the mid-deck plate and outside the drain pipes. This component consists of 1 volume (Volume 21-01) and 2 junctions (Junctions 21-01 and 21-02). The Volume 27-01 is corresponding the Node 21 of the TRANFLO model given in Reference 1. As given in the Table 4.2.2 of Reference 1, the flow area and volume size for the Node 21 are 152.19 ft<sup>2</sup> and 347.0 ft<sup>3</sup>. The volume length of Node 21 is 347.0/152.19 = 2.281 ft. The flow area and volume length are specified as input data while the volume size is not specified which will be calculated by the code using the volume length and flow area.

The Volume 21-01 is a vertical upward volume. The inclination angle is 90° and the elevation change is same as the volume length. The hydraulic diameter of the volume is not specified also and the code will calculate it.

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The initial water properties for Node 21 are given in Reference 1 as pressure at 1021.12 psia, temperature at 547°F and void fraction of 1.0 (pure steam). Since there is no superheated steam in the steam generator, the steam in volume 21-01 must be saturated steam. For saturated steam, the RELAP5 code does not allow to specify both the water pressure and temperature. The steam pressure of TRANFLO Node 21 is used for this component. The initial water properties are specified as pressure at 1021.12 psia and the quality of 1.0.

The Junction 21-01 connects the outlet of Volume 21-01 to the inlet of Volume 20-01 which is corresponding to the Connector 25 of the TRANFLO model. The smaller of the two flow areas of Volumes 21-01 and 20-01 is 70.75  $ft^2$  which is used as the flow area for this junction. As given in the Reference 1, no flow resistance is specified for the Connector 25. However, a abrupt flow area change is specified for the Connector 25. Therefore, a forward and reverse flow resistant coefficient of 0.0 is used for this junction and the junction control flag a is set to 1 to specify a abrupt area change at this junction.

The Junction 21-02 connects the inlet of Volume 21-01 to the inlet of Volume 53-01 which is corresponding to the Connector 41 of the TRANFLO model. As given in the Reference 1, the smallest flow area of the three segments of the Connector  $\frac{26}{100}$  is 7.96 ft<sup>2</sup> and a forward and reverse flow 41

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SUBJECT	loads on	the Steam, Generator	Support Plats	During SLB Accident
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resistant coefficients of 1.78 and 1.67 are associated with this flow area. The following input are used for the Component 21. branch 0210000 abovspr 1 0210001 2 00000 0.0 0.0 0. 90. 2.281 0.00015 152.19 2.281 0210101 fe 10/2/96 1441 10/1/96 1.0 2 1021.12 0210200 021010000 02000000 70.75 0.0 000100 0.0 0211101 000000 021000000 053000000 7.96 1.67 1.78 0212101 0.0 0211201 0.0 0.0 0212201 0.0 0.0 0.0

#### Component 20

The Component 20 is a single volume with assigned name spsteam which is used to model the region outside the upper and lower secondary separator. This component consists of 1 volume (Volume 20-01). The Volume 20-01 is corresponding the Node 20 of the TRANFLO model given in Reference 1. As given in the Table 4.2.2 of Reference 1, the flow are and volume size for the Node 20 are 70.75 ft<sup>2</sup> and 527.1 ft<sup>3</sup>. The volume length of Node 20 is 527.1/70.75 = 7.4502 ft. The flow area and volume length are specified as input data while the volume size is not specified which will be calculated by the code using the volume length and flow area.

GENERAL COMPUTATION SHEET	SHEET NO.35 OF/74 SHEETS CALC NO. STA-042 8.0
SUBJECT Loads on the Steam Generator Support	Plats During SLB Accident
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The Volume 20-01 is a vertical upward volume. The inclination angle is 90° and the elevation change is same as the volume length. The hydraulic diameter of the volume is not specified also and the code will calculate it.

The initial water properties for Node 20 are given in Reference 1 as pressure at 1020.96 psia, temperature at 547°F and void fraction of 1.0 (pure steam). Since there is no superheated steam in the steam generator, the steam in volume 20-01 must be saturated steam. For saturated steam, the RELAP5 code does not allow to specify both the water pressure and temperature. The steam pressure of TRANFLO Node 20 is used for this component. The initial water properties are specified as pressure at 1020.96 psia and the quality of 1.0.

The following input are used for the Component 20. 0200000 spsteam snglvol 00000 7.4502 0.0 0. 90. 7.4502 0.00015 0.0 0200101 70.75 1020.96 1.0 0200200 2

#### Component 19

The Component 19 is a separator with assigned name dryer which is used to model the region inside the secondary separator peerless vane banks. This component consists of 1 volume (Volume 19-01) and 3 junctions

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SHEET NO 69 OF 74 SHEETS

400.0	55.2607
600.0	54.9895
800.0	54.7069
1000.0	54.3982
1200.0	54.0907
1400.0	53.7516

Each of the primary side volume (Component 1) connects to one heat slab as the left boundary volume. The left boundary volumes for the heat slabs 1 to 60 are Volumes 1-01 to 1-60. Due to the U-shape tubes, each secondary side volume (Components 30 and 2) connects to two heat slabs as the right boundary volume, once to the hot-leg side tubes and once to the cold-leg side tubes. The right boundary volumes for the heat slabs 1 to 60 are Volumes 30-01, 2-01 to 2-29, 2-29 to 2-01 and 30-01. The heat transfer area for each heat slab is linearly dependent on the length of heat slab which is equal to the length of the left and right boundary volumes. The heat transfer area given for the Heat Connector 1 of the TRANFLO model, which is the heat transfer area for the left side of the heat Node 1, is 2874.2 ft<sup>2</sup> with the volume length of 50.5" (or 4.2083 ft) for Node 1. Therefore, the heat transfer area per foot of the primary side volume length can be calculated as 2874.2/4.2083 = 682.9 ft<sup>2</sup>. The heat transfer area to the left boundary volumes cab calculated as follows.

For Heat Slabs 1 and 60, the length of the left boundary Volumes 1-01 and

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transfer analysis. Then, the interval between all the 11 meshes equals to 0.00438/10 = 0.000438 ft. Since the initial water temperature at both the primary and secondary sides of the tubes is 547°F, the initial temperatures of all 11 mesh points are 547°F.

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As given in the Reference 1, the tube material is inconel 600. The thermal property of the inconel 600 is given in Reference 5 which is input to the RELAP5 model as an user specified table (for composite 1). The thermal conductivity and volumetric heat capacity of inconel 600 are listed as follows.

Temperature (°F)	Thermal Conductivity (btu/s*ft*°F)
70.0	2.3843e-03
200.0	2.5232e-03
400.0	2.8009e-03
600.0	3.0787e-03
800.0	3.3565e-03
1000.0	3.6574e-03
1200.0	3.9815e-03
1400.0	4.3056e-03

Temperature (°F)	Volumetric Heat Capacity (btu/ft³*°F)
70.0	55.6831
200.0	55.5227

#### SHEET NO.<u>67</u> OF**174** SHEETS CALC NO.\_\_\_\_\_STA-042 <u>**R**.0</u> ts During SLB Accident

SUBJECT Loads on the Steam Generator Support Plats During SLB Accident MADE BY <u>H M Lee</u> DATE <u>10/1/96</u> CHECK BY <u>L R Chang</u> APPROVED BY

5010000	prmout	: tmdj	pjun		
5010101	101000	0 1010	00000	10.956	
5010200	1				
5010201	0.0	9148.5	0.0	0.0	
5010202	1.0e6	9148.5	0.0	0.0	

#### <u>Heat Slabs</u>

The heat slabs are used to model the steam generator tubes and provide heat transfer from the primary side of the tubes to the secondary side of the tubes. There are total 60 heat slabs modeled. Each heat slab connects one primary side volume (Component 1) and one secondary side volume (Component 2). The hydraulic diameter for Volumes 1-01 to 1-60 is 0.0642 ft which is the inside diameter of the tubes. The inside radius of the tubes is 0.0321 ft. Therefore, the left boundary coordinate for each of the heat slabs is 0.0321 ft. The tube is cylindrical shape.

The mesh location is provided by the input. As given in the heat structure input for the TRANFLO model, the distance of heat transfer for each heat connector is 0.00219 ft which equals to the half of the tube thickness. The tube thickness is 2\*0.00219 = 0.00438 ft. In the RELAP5 model, 11 radial mesh points are used to model the tube wall for the heat

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This component consists of 1 time dependent junction (Junction 500). The Junction 500 connects the Volume 100-01 to the Volume 1-01. The flow area of the junction equals to the flow area of the Volume 1-01 which is  $10.956 \text{ ft}^2$ . As discussed in the Section 2, a constant mass flow rate of 9148.5 lb/sec is assumed through the junction.

The following input are used for the Component 500.

tmdpjun 5000000 prminl 10.956 1000000 100000000 5000101 5000200 1 0.0 0.0 9148.5 5000201 0.0 0.0 0.0 9148.5 1.0e6 5000202

#### Component 501

The Component 501 is a time-dependent junction with assigned name prmout which is used to provide constant flow out the primary side of the tubes. This component consists of 1 time dependent junction (Junction 501). The Junction 501 connects the Volume 1-60 to the Volume 101-01. The flow area of the junction equals to the flow area of the Volume 1-60 which is  $10.956 \text{ ft}^2$ . As discussed in the Section 2, a constant mass flow rate of 9148.5 lb/sec is assumed flow out the primary side of the tubes.

The following input are used for the Component 501.

dependent volume (Volume 101-01). Since the volume size and length of the Volume 100-01 does not affect the calculation, an arbitrary volume size of 5000 ft<sup>3</sup> and an arbitrary volume length of 10 ft are used for the Volume 101-01.

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Since the flow rate is controlled by the time dependent junctions, Components 500 and 501, the pressure of the Volume 101-01 does not affect on the primary side flow calculation. There is no reverse flow in the primary side of the tubes. The temperature does not have any impact on the calculation. Therefore, the pressure in the volume 101-01 is set at slightly lower the pressure at the Volume 100-01 and the temperature of the Volume 101-01 is set at the same temperature of the Volume 100-01. The following input are used for the Component 101. 1010000 outplen tmdpvol 0.0 0 0.0 0.0 1010101 0.0 10.0 5000.0 0.0 0.0 1010200 3 2200.0 1010201 0.0 547.0 1010202 5.0 2200.0 547.0 1010203 15.0 700.0 491.0

#### Component 500

The Component 500 is a time-dependent junction with assigned name prminl which is used to provide constant flow to the primary side of the tubes.

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 Image: Comparison of the steam Generator Support Plats During SLB Accident

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the primary water pressure during the transient run. In addition, since the primary water flow rate is fixed by the time dependent junctions, the primary side pressure has negligible effect on the heat transfer calculation. Therefore, this discrepancy has no impact on this analysis.

As given in the Reference 1, the primary water temperature is 547°F at the initiation of the steam line break and the temperature then is reduced by 112°F in 20 seconds or 56°F in 10 seconds. The temperature for Volume 100-01 is specified as 547°F from time 0.0 second to 5.0 seconds (steady state run) and then reduced to 491°F at time 15 seconds.

The following input are used for the Component 100. inplen tmdpvol 1000000 0 0.0 0.0 0.0 0.0 0.0 5000.0 10.0 0.0 1000101 1000200 3 547.0 2235.7 1000201 0.0 547.0 2250.0 1000202 5.0 1000203 15.0 800.0 491.0

#### Component 101

The Component 101 is a time-dependent volume with assigned name outplen which is used as a mass sink. This component consists of 1 time

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0011301 9148.5 0.0 0.0 59

#### Component 100

The Component 100 is a time-dependent volume with assigned name inplen which is used as a mass source at preset condition for the primary side tubes (Component 1). This component consists of 1 time dependent volume (Volume 100-01). Since the volume size and length of the Volume 100-01 does not affect the calculation, an arbitrary volume size of 5000 ft<sup>3</sup> and an arbitrary volume length of 10 ft are used for the Volume 100-01.

Since the flow rate is controlled by the time dependent junctions, Components 500 and 501, the pressure of the Volume 100-01 does not affect on the primary side flow calculation. As given in the Reference 1, the primary side pressure is 2250 psia at the initiation of the steam line break and the primary side pressure is reduced by 1450 psi in 10 seconds. Since the steam line break is initiated at 5 seconds in the RELAP5 analysis, the time history for the pressure is set at 2250 psia for the first 5 seconds of the run and then reduced to 800 psia in the next 10 seconds. A pressure of 2235.7 psia instead of 2250 psia is input for the Volume 100-01 at 0.0 second. The pressure is increased to 2250 psia at 5 seconds and then reduced to 800 psia from 5 seconds to 15 seconds as the pressure specified in the TRANFLO model. This slightly lower primary side water pressure during the 5 seconds steady state run does not affect

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0010316	3.0	31			
0010317	0.5	33			
0010318	1.60435	35			
0010319	0.5	37			
0010320	1.60435	39			
0010321	0.5	41			
0010322	1.60435	43			
0010323	0.5	45			
0010324	1.60435	47			
0010325	0.5	49			
0010326	1.60435	51			
0010327	0.5	53			
<b>0</b> 010328	1.60435	55			
0010329	0.5	57			
0010329	1.2553	59			
0010330	1.1667	60			
0010601	90.0	30			
0010602	-90.0	60			
0010801	0.0	0.0642 60			
0011001	00000	60			
0011101		59			
0011201	3 <b>1</b> 25	0.0 547.0	0.0	0.0	0.0
0011300	1	HML 191/96 Fe 192/96			
		Fe 10/2/96			

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junctions. As discussed in Section 4, a constant primary side mass flow rate of 9148.5 lb/sec is assumed. The initial mass flow rate of 9148.5 1b/sec is used for all the 59 junctions.

The follow	wing inpu <sup>.</sup>	t are used	for	the	Component 🗲	14ML 10/1/96 Le 19496
0010000	tubes	pipe				Le 10/2/96
0010001	60					
0010101	10.956	60				
0010301	1.1667	1				
0010302	1.2553	3				
0010303	0.5	5				
0010304	1.60435	7				
0010305	0.5	9				
0010306	1.60435	11				
<b>0</b> 010307	0.5	13				
0010308	1.60435	15				
0010309	0.5	17				
0010310	1.60435	19				
0010311	0.5	21				
0010312	1.60435	23				
0010313	0.5	25				
0010314	1.60435	27				
0010315	0.5	29				

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Volume 2-29. This small discrepancy does not have significant effect on the total heat transfer from the primary side to the secondary side and the effect on the loads on the TSPs is negligible.

The Volumes 1-01 to 1-30 are vertical upward volumes. The inclination angles are 90° and the elevation changes are same as the volume lengths. The Volumes 1-30 to 1-60 are vertical downward volumes. The inclination angles are -90° and the elevation changes are same as the volume lengths. The TRANFLO code specifies the hydraulic diameter of a control volume in the input for a connector. The hydraulic diameter of 0.0642 ft is specified for the Connectors 1 to 17 of the TRANFLO model. The same hydraulic diameter is used for the volumes 1-01 to 1-60. Since a constant flow rate is assumed for the primary side of the tubes during the entire transient, the friction loss in the primary side of the tubes is not important. A smooth wall is assumed for the Volumes 1-01 to 1-60. The initial pressure of 2250 psia and temperature of 547 °F are used for the Node 1 to 16 of the TRANFLO model, the same initial pressure and temperature are used for the Volumes 1-01 to 1-60.

There are 59 junctions, Junctions 1-01 to 1-59, used in the Component 1 to connect the 60 volumes of the Component 1. The junction flow area for the 59 junctions is same as the flow area for the volumes which is 10.956 ft<sup>2</sup>. Since the tubes are smooth, no flow resistance is used for the

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The length of Volumes 1-10 and 1-51 equals to the length of Volume 2-09. The length of Volumes 1-11 and 1-50 equals to the length of Volume 2-10. The length of Volumes 1-12 and 1-49 equals to the length of Volume 2-11. The length of Volumes 1-13 and 1-48 equals to the length of Volume 2-12. The length of Volumes 1-14 and 1-47 equals to the length of Volume 2-13. The length of Volumes 1-15 and 1-46 equals to the length of Volume 2-14. The length of Volumes 1-16 and 1-45 equals to the length of Volume 2-15. The length of Volumes 1-17 and 1-44 equals to the length of Volume 2-16. The length of Volumes 1-18 and 1-43 equals to the length of Volume 2-17. The length of Volumes 1-19 and 1-42 equals to the length of Volume 2-18. The length of Volumes 1-20 and 1-41 equals to the length of Volume 2-19. The length of Volumes 1-21 and 1-40 equals to the length of Volume 2-20. The length of Volumes 1-22 and 1-39 equals to the length of Volume 2-21. The length of Volumes 1-23 and 1-38 equals to the length of Volume 2-22. The length of Volumes 1-24 and 1-37 equals to the length of Volume 2-23. The length of Volumes 1-25 and 1-36 equals to the length of Volume 2-24. The length of Volumes 1-26 and 1-35 equals to the length of Volume 2-25. The length of Volumes 1-27 and 1-34 equals to the length of Volume 2-26. The length of Volumes 1-28 and 1-33 equals to the length of Volume 2-27. The length of Volumes 1-29 and 1-32 equals to the length of Volume 2-28. The length of Volumes 1-30 and 1-31 equals to the length of Volume 2-29. However, a volume length of 3.0 ft is input for the Volumes 1-30 and 1-31 which is slightly shorter than the volume length of 3.2075 ft for the

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30 volumes (Volumes 30-01, 2-01 to 2-29). There is no heat transfer from primary side to secondary side is modeled for the Volume 2-30. Since the U-tubes are used in the Model 51 steam generator, 60 volumes (Volumes 1-01 to 1-60) are needed to model the primary side of the tubes which are included in the Component 1. To connect the 60 volumes, 59 junctions (Junction 1-01 to 1-59) are also included in the Component 1.

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The flow area for the primary side of the tubes used in the TRANFLO model can be calculated as the volume size of Node 1 (46.11 ft<sup>3</sup>) divided by the flow length of Node 1 (50.5" or 4.2083 ft): 46.11/4.2083 = 10.956 ft<sup>2</sup>. This flow area is used for all the volumes of the Component 1. To achieve correct heat transfer from the primary side to the secondary side, the volume lengths of Volumes 1-01 to 1-60 have to be same as the following volumes:

The length of Volumes 1-01 and 1-60 equals to the length of Volume 30-01. The length of Volumes 1-02 and 1-59 equals to the length of Volume 2-01. The length of Volumes 1-03 and 1-58 equals to the length of Volume 2-02. The length of Volumes 1-04 and 1-57 equals to the length of Volume 2-03. The length of Volumes 1-05 and 1-56 equals to the length of Volume 2-04. The length of Volumes 1-06 and 1-55 equals to the length of Volume 2-05. The length of Volumes 1-07 and 1-54 equals to the length of Volume 2-06. The length of Volumes 1-08 and 1-53 equals to the length of Volume 2-07. The length of Volumes 1-09 and 1-52 equals to the length of Volume 2-08.

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the high loads on the TSPs only last less than 1 second after the steam line break is initiated, the heat added to the secondary side is very small during that period which does not have significant effect on the analysis results. Therefore, accurate modeling of the primary loop is not required.

As discussed in Section 2, a constant mass flow through the primary side of the tubes during the entire transient is assumed. To achieve the constant mass flow in the primary loop, two time dependent junction, Components 500 and 501, are used to provide constant mass flow rate through the entire transient. The Component 100 is used as a mass source while the Component 101 is used a mass sink. The Component 1 is used to model the primary side of the tubes.

#### Component 1

The Component 1 is a Pipe with assigned name tubes which is used to model the region inside (primary side) the steam generator tubes. In the TRANFLO model, the primary side of the steam generator tubes is modeled by the Nodes 1 to 16 and the Connectors 2 to 16. In the RELAP5 model, To provide correct heat transfer from primary side to the secondary side, the lengths of the volumes modeling the primary side have to be same as the lengths of the volumes modeling the secondary side of the tube region. The secondary side of the steam generator tubes are modeled by

_	ECT <u>Load</u> BY <u>I</u> AA	is on the	Stear TE_/9	n Gener 1/96	CHE	r Sup CK Bi	oport P (	lats [	C NO <u>Jurin</u> APPR	g SLE OVED	Accide	22 <u>R</u>
	The follo	owing inp	ut are	e used	for	the	Compon	ent 3	5,	Hml Se	10/1/46	
	0350000	downc	pipe	5							(Jeles	
,	0450001	3										
2 2 9 <sup>1</sup>	0350101	0.0	3									
(	0350201	7.096	2									
	0350301	11.827	3									
	0350401	122.4	3									
	<b>0350</b> 601	-90.0	3									
	0350801	0.00015	0.	4275	3							
	0351001	00000	3									
	0351101	000000	2									
	0351201	3 102	4.84	547.0	0	0.0	0.0	0.0	1			
	0351202	3 102	8.64	547.0	0	0.0	0.0	0.0	2			
	0351203	3 103	2.44	547.0	0	0.0	0.0	0.0	3			
	0351300	1										

0351301 0.0 0.0 0.0 2

#### Primary Loop

The primary loop includes the components 1, 100, 101, 500 and 501. A schematic of the secondary loop is shown in the Figure 5-3. The primary loop is only used to provide heat source to the secondary side. Since

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used for the Volumes 35-01, 35-02 and 35-03. The initial pressure in the Volumes 35-01, 35-02 and 35-03 can be calculated as: The initial pressure at the center of the Volume 30-01 = 1034.15 psia The elevation increase from the center of the Volume 30-01 to the center of the Volume 35-03 = 11.827/2 - 1.1667/2 = 5.3302 ft. As calculated for the Component 2, the water static pressure reduces 46.17/144 = 0.3206 psi for every foot elevation increase. Then, the initial pressure at the center of the Volume 35-03 is 1034.15 - 0.3206 \* 5.3302 = 1032.44 psia. The elevation increase from the center of the Volume 30-03 to 30-02 or  $1 \le 1.4714$ from the center of The Volume 30-02 to 30-01 is 11.827 ft. Then, the initial pressure at the center of the Volume 30-02 is  $1032.44 - 0.3206 \times 10.47146$ from the center of The Volume 30-02 to 30-02 is  $1032.44 - 0.3206 \times 10.47146$ initial pressure at the center of the Volume 30-02 is  $1032.44 - 0.3206 \times 10.47146$ initial pressure at the center of the Volume 30-02 is  $1032.44 - 0.3206 \times 10.47146$ initial pressure at the center of the Volume 30-02 is  $1032.44 - 0.3206 \times 10.47146$ initial pressure at the center of the Volume 30-02 is  $1032.44 - 0.3206 \times 10.47146$ initial pressure at the center of the Volume 30-02 is  $1032.44 - 0.3206 \times 10.47146$ The elevation increase from the center of the Volume 30-02 is  $1032.44 - 0.3206 \times 10.47146$ initial pressure at the center of the volume 30-02 is  $1032.44 - 0.3206 \times 10.47146$ A state of the volume initial pressure at the center of the volume initial pressure initial pr

Volume 30-01 is 1028.64 - 0.3206 \* 11.827 = 1024.84 psia.  $\mu_{ml} / 0//66$ 

The Junction 35-01 connects the Volume 35-01 to the Volume 35-02 and the Junction 35-02 connects the Volume 35-02 to the Volume 35-03. Since the majority portion of the downcomer has flow area of 7.096  $ft^2$ , the flow area of the Junctions 35-01 and 35-02 is set to be 7.096  $ft^2$ . There is no abrupt area change and flow element in the downcomer. Therefore, no flow resistance is specified for the Junctions 35-01 and 35-02. The smooth area change is also used for these junctions.

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The reason is the flow area in the downcomer region is not constant and the flow area of 7.096 ft<sup>2</sup> only represents the majority portion of the downcomer. Since the propagation of the depressurization wave due to steam line break has significant effects on this analysis, the volume length has to be preserved. The initial water inventory in the steam generator also affects the analysis. Therefore, the downcomer length and volume are preserved in this analysis. The volume length for each of the three volumes can be calculated as 35.48/3 = 11.827 ft. The volume size for each of the three volumes can be calculated as 367.22/3 = 122.4 ft<sup>3</sup>. Here The volume length and size are specified as input data while the flow area is not specified which will be calculated by the code using the volume length and size.

The Volumes 35-01, 35-02 and 35-03 are vertical downward volumes. The inclination angles are -90° and the elevation changes are same as the volume lengths. The TRANFLO code specifies the hydraulic diameter of a control volume in the input for a connector. The hydraulic diameter of 0.4275 ft is used for the segment 1 of the Connectors 30 and 31 and segment 2 of the Connectors 29 and 43 of the TRANFLO model. The same hydraulic diameter is used for the volumes 35-01, 35-02 and 35-03.

As given in Reference 1, the Nodes 35 and 37 of the TRANFLO model contain single phase water initially. The water temperature is 547 °F which is

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The Junction 34-01 connects the outlet of Volume 34-01 to the inlet of Volume 35-01. Since the Nodes 35 and 37 of TRANFLO model are combined in the RELAP5 model, the Junction 34-01 is corresponding to the combination of the Connectors 29 and 43. The smaller of the two flow areas of Volumes 34-01 and 35-01 is 7.096  $ft^2$  which is used as the flow area for this junction. As given the Reference 1, no flow resistance is specified for the Connectors 29 and 43. However, an abrupt area change is specified for the Connectors 29 and 43. Therefore, the forward and reverse flow resistant coefficient of 0.0 is used for this junction and the control flag a is set to 1 to specify an abrupt area change at this junction.

HAL 19/1/96 Le 11/2/96 The following input are used for the Component  $3\beta$ . 0340000 feedra branch 1 0340001 1 00000 3.1097 0.0 0. -90. -3.1097 0.00015 0.0 0340101 92.1 1022.48 547.0 0340200 3 032010000 035000000 7.096 0.0 0.0 000100 0341101 0341201 0.0 0.0 0.0

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Component 35

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The Component 35 is a Pipe with assigned name downc which is used to model the downcomer region. In the TRANFLO model, the downcomer region is modeled by two Nodes, Node 35 for hot-leg downcomer and Node 37 for cold-leg downcomer. Since the feedwater is not included in the RELAP5 model and the heat transfer from primary side to the secondary side is insignificant for this analysis due to the short duration, the Nodes 35 and 37 of the TRANFLO model are combined in the RELAP5 model. However, due to the long length of the downcomer, the downcomer region is separated into three volumes with equal the volume lengths. There are 3 volumes (Volumes 35-01, 35-02 and 35-03) and 2 junctions (Junctions 35-01 and 35-02) included in the Component 35.

As given in the Reference 1, the combined flow area of the Nodes 35 and 37 of the TRANFLO model is  $3.548 \times 2 = 7.096$  ft<sup>2</sup>. The combined volume size of the Nodes 35 and 37 of the TRANFLO model is  $183.6 \times 2 = 367.2$ ft<sup>3</sup>. The segment 1 of the Connectors 30 and 31 and segment 2 of the Connectors 29 and 43 have the same segment length of 17.74 ft. This indicates that the half of the downcomer length (or the volume lengths for Nodes 35 and 37) is 17.74 ft and the downcomer length is 2\*17.74 = 35.48 ft. However, a discrepancy is noticed. The volume size based on the combined flow area of 7.096  $ft^2$  for the Nodes 35 and 37 and volume length of 35.48 ft is 7.096 \* 35.48 = 251.77 ft<sup>3</sup> which is smaller than the combined size of the Nodes 35 and 37 as given in the Reference 1.

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0332201 0.0 0.0 0.0

#### Component 34

The Component 34 is a branch with assigned name feedrg which is used to model the region from feedring to top of the tube sheet downcomer, the region outside feedring and primary separator risers. This component consists of 1 volume (Volume 34-01) and 1 junction (Junctions 34-01). The Volume 34-01 is corresponding the Node 34 of the TRANFLO model given in Reference 1. As given in the Table 4.2.2 of Reference 1, the flow are and volume size for the Node 34 are 92.1 ft<sup>2</sup> and 286.4 ft<sup>3</sup>. The volume length of Node 36 is 286.4/92.1 = 3.1097 ft. The flow area and volume length are specified as input data while the volume size is not specified which will be calculated by the code using the volume length and flow area.

The Volume 34-01 is a vertical downward volume. The inclination angle is -90° and the elevation change is same as the volume length. The hydraulic diameter of the volume is not specified also and the code will calculate it.

The initial water properties for the Node 34 of the TRANFLO model are single phase liquid at pressure of 1022.48 psia and temperature of 547 °F which are also used for the Volume 34-01.

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Volume 33-01 which is corresponding to the Connector 28 of the TRANFLO model. The smaller of the two flow areas of Volumes 32-01 and 33-01 is  $17.35 \, \text{ft}^2$  which is used as the flow area for this junction. As given the Reference 1, no flow resistance is specified for the Connector 28. Therefore, the forward and reverse flow resistant coefficient of 0.0 is used for this junction.

The Junction 33-02 connects the outlet of Volume 33-01 to the inlet of Volume 34-01 which is corresponding to the Connector 23 of the TRANFLO model. As given in the Reference 1, the smallest flow area of the two segments of the Connector 23 is  $79.288 \text{ ft}^2$  which is used as the flow area for this junction. As given the Reference 1, no flow resistance is specified for the Connector 23. Therefore, a forward and reverse flow resistant coefficient of 0.0 is used for this junction.

The follo	wing input are used for the Component 33.	
0330000	abovfl branch	
0330001	2 1	
0330101	100.79 2.9225 0.0 0902.9225 0.00015 0.0 00000	
0330200	2 1021.72 0.73	
0331101	032010000 033000000 17.35 0.0 0.0 000000	
0332101	033010000 034000000 79.288 0.0 0.0 000000	
0331201	0.0 0.0 0.0	

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The Component 33 is a branch with assigned name abovfl which is used to model the lower portion of the region below the mid-deck plate and above the feedring including the region outside the drain pipes, separator downcomer and separator riser. This component consists of 1 volume (Volume 33-01) and 2 junctions (Junctions 33-01 and 33-02). The Volume 33-01 is corresponding the lower part of Node 33 of the TRANFLO model given in Reference 1. The flow area of Volume 33-01 is 100.7 ft<sup>2</sup> which is same as the flow area for Volume 53 or the Node 33 of TRANFLO model. As discussed for the Component 53, the volume length of Volume 33-01 should be 2.9225 ft. The flow area and volume length are specified as input data while the volume size is not specified which will be calculated by the code using the volume length and flow area.

The Volume 33-01 is a vertical downward volume. The inclination angle is -90° and the elevation change is same as the volume length. The hydraulic diameter of the volume is not specified also and the code will calculate it.

The initial water properties for Volume 33-01 are same as those for the Volume 53-01 which are two-phase water at pressure of 1021.72 psia and quality of 0.73.

The Junction 33-01 connects the outlet of Volume 32-01 to the inlet of

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model. The smaller of the two flow areas of Volumes 36-01 and 53-01 is 2.34 ft<sup>2</sup> which is used as the flow area for this junction. As given the Reference 1, a forward and reverse flow resistant coefficient of 0.5 associated with a flow area of 2.34 ft<sup>2</sup> for segment 1 of the Connector 22 which is also used for the Junction 53-01.

The Junction 53-02 connects the outlet of Volume 53-01 to the inlet of Volume 33-01. This junction is created due to splitting the Node 33 of TRANFLO model into two volumes in RELAP5 model. There is no connector in the TRANFLO model corresponding to this junction. The flow area of this junction is same as the flow area of the Volumes 53-01 and 33-01 (100.7 ft<sup>2</sup>) and no flow resistance is specified for this junction. The following input are used for the Component 53. abovfr2 branch 0530000 HAL 19/196 Fe 10/2/96 0530001 1 2 100.7% 3.9156 0.0 0. -90. -3.9156 0.00015 00000 0.0 0530101 1021.72 0.73 0530200 2 000000 036010000 053000000 2.34 0.5 0.5 0531101 0.0 0.0 000000 053010000 033000000 100.7 0532101 0.0 0.0 0.0 0531201 0.0 0.0 0.0 0532201

Component 33

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688.6/100.7 = 6.8381 ft. The top 3.9156 portion of the volume length for Node 33 is used for the Volume 53-01. Then, the remaining 2.9225 ft of the volume length for Node 33 is used for the volume length of Volume 33-01. The flow area and volume length are specified as input data while the volume size is not specified which will be calculated by the code using the volume length and flow area.

The Volume 53-01 is a vertical downward volume. The inclination angle is -90° and the elevation change is same as the volume length. The hydraulic diameter of the volume is not specified also and the code will calculate it.

The initial water properties for Node 33 are given in Reference 1 as pressure at 1021.72 psia, temperature at 547°F and void fraction of 0.73. For a two-phase water, the RELAP5 code does not allow to specify both the water pressure and temperature. The pressure of TRANFLO Node 33 is used for this component. As discussed for the Component 23, the void fraction of 0.73 is used in the RELAP5 analysis as quality for this volume. The initial water properties are specified as pressure at 1021.72 psia and the quality of 0.73.

The Junction 53-01 connects the outlet of Volume 36-01 to the inlet of Volume 53-01 which is corresponding to the Connector 22 of the TRANFLO

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#### Component 53

The Component 53 is a branch with assigned name abovfr2 which is used to model the upper portion of the region below the mid-deck plate and above the feedring including the region outside the drain pipes, separator downcomer and separator riser. This component consists of 1 volume (Volume 53-01) and 2 junctions (Junctions 53-01 and 53-02). The Volume 53-01 is corresponding the upper part of Node 33 of the TRANFLO model Since the RELAP5 code only allows the junctions given in Reference 1. located either at the inlet of the volume or the outlet of the volume, the Node 33 of TRANFLO model has to be separated to two volumes in the RELAP5 model, Volumes 53-01 and 33-01. Otherwise, the drain water from the primary separator (Component 22) can not be connected to the drain return at the correct elevation. As given in the Table 4.2.2 of Reference 1, the flow are and volume size for the Node 33 are 100.7  $ft^2$ and 688.6 ft<sup>3</sup>. The elevation of the drain water outlet junction from the 2  $J^{\mu}$   $J^{\mu}$   $J^{\mu}$   $J^{\mu}$   $J^{\mu}$   $J^{\mu}$   $J^{\mu}$  primary separator (Junction 22-03) is at 39.7188 ft above the center of Volume 2-01 (as given in the output of the RELAP5 analysis) which is same as the elevation of the outlet of the Volume 32-01 (or Junction 33-01). The elevation at the outlet of the Volume 36 (Junction 53-01) is 43.5344 ft above the center of the Volume 2-01. Therefore, to make the elevation at the outlet of the Volume 53-01 (or Junction 53-02) at 39.7188 ft above the center of the Volume 2-01, the volume length for the Volume 53 has to be 43.6344 - 39.7188 = 3.9156 ft. The volume length of Node 36 is

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significant effects on the analysis. The flow area and volume length are specified as input data while the volume size is not specified which will be calculated by the code using the volume length and flow area input.

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The Volume 36-01 is a vertical downward volume. The inclination angle is -90° and the elevation change is same as the volume length. The hydraulic diameter of the volume is not specified also and the code will calculate it.

The initial water properties for Node 36 are given in Reference 1 as pressure at 1021.57 psia, temperature at 547°F and void fraction of 0.82. For a two-phase water, the RELAP5 code does not allow to specify both the water pressure and temperature. The pressure of TRANFLO Node 36 is used for this component. As discussed for the Component 23, the void fraction of 0.82 is used in the RELAP5 analysis as quality for this volume. The initial water properties are specified as pressure at 1021.57 psia and the quality of 0.82.

The following input are used for the Component 36. 0360000 spsteam snglvol 0360101 2.34 9.7312 0.0 0. -90. -9.7312 0.00015 0.0 00000 0200200 2 1021.57 0.82

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Since the steam flow through is break is chocked through the entire transient, the initial condition for the Volume 38-01 does not affect the analysis. Saturated steam at atmospherical pressure (14.7 psia) is assumed for the Volume 38-01.

The following input are used for the Component 38. 0380000 contnm snglvol 00000 0.0 10000.0 200.0 0.0 0.0 90.0 200.0 0.00015 0380101 1.0 0380200 2 14.7

#### Component 36

The Component 36 is a single volume with assigned name dsdryer which is used to model the secondary separator drain pipes. This component consists of 1 volume (Volume 36-01). The Volume 36-01 is corresponding the Node 36 of the TRANFLO model given in Reference 1. As given in the Table 4.2.2 of Reference 1, the flow are and volume size for the Node 36 are 2.34 ft<sup>2</sup> and 22.83 ft<sup>3</sup>. The volume length of Node 36 is 22.83/2.34 =9.7564 ft. However, since the TRANFLO code does not require perfect elevation match for its Nodes, the use of the volume length of 9.7564 ft causes a small elevation discrepancy at the junction connects the Volume 36-01. Therefore, the volume length of 9.7312 ft is used the Volume 36-01 (equivalent 0.059 ft<sup>3</sup> volume reduction). The small volume length discrepancy on the water drain return from the dryer does not cause any

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The following input are used for the Component 518. 5180000 break valve 000100 017010000 038000000 4.6 0.0 0.0 5180101 5180110 0.0 0.0 1.0 1.0 5180201 0.0 0.0 0.0 1 5180300 mtrvlv 502 503 1000.0 0.0 5180301

#### Component 38

The Component 38 is a single volume with assigned name contnm which is used to provide a mass sink for steam blowdown after the break is initiated. This component consists of 1 volume (Volume 38-01). Since the steam flow through the break is choked through the entire transient, a arbitrary large flow area of 10000.0 ft<sup>2</sup> and volume length of 200.0 ft are used. The flow area and volume length are specified as input data while the volume size is not specified which will be calculated by the code using the volume length and flow area.

The Volume 38-01 is a vertical upward volume. The inclination angle is 90° and the elevation change is same as the volume length. The hydraulic diameter of the volume is not specified also and the code will calculate it.

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The Component 518 is a valve junction with assigned name break which is used to simulate the steam line break. This component consists of 1 valve junction (Junction 518) which provides a flow control from the Volume 17-01 (Component 17) to the Volume 38-01 (Component 38). The Junction 518 is corresponding the Connector 18 of the TRANFLO model given in Reference 1.

For this case, the location of the steam line break is assumed at the steam nozzle which has an inside diameter of 29" (Ref. 7). The flow area of the Junction 518 can be calculated as  $(29/24)^2 * 3.1416 = 4.6 \text{ ft}^2$ . Since the flow through this junction is always chocked during the entire transient, no flow resistance is assigned to this junction. However, an abrupt area change at this junction is used by setting the junction control flag a to 1. The RELAP5 motor valve is **set to** open the motor valve (Initiate steam line break). The valve is initially closed and no steam is **blew** out from the steam generator until the Trip 502 is tripped. Since it is assumed the steam line break open at very high speed, a 0.001 second valve opening time (or a valve change rate of 1000 second<sup>-1</sup>) is assumed. The Trip 503 is set to close the motor valve. Since the steam line break can not be terminated, an arbitrary long time is used for the Trip 503.

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as input data while the volume size is not specified which will be calculated by the code using the volume length and flow area.

The Volume 17-01 is a vertical upward volume. The inclination angle is 90° and the elevation change is same as the volume length. The hydraulic diameter of the volume is not specified also and the code will calculate it.

The initial water properties for Node 17 are given in Reference 1 as pressure at 1020.94 psia, temperature at 547°F and void fraction of 1.0 (pure steam). Since there is no superheated steam in the steam generator, the steam in volume 17-01 must be saturated steam. For saturated steam, the RELAP5 code does not allow to specify both the water pressure and temperature. The steam pressure of TRANFLO Node 17 is used for this component. The initial water properties are specified as pressure at 1020.94 psia and the quality of 1.0.

The following input are used for the Component 17. 0170000 sgdoom snglvol 0170101 94.12 3.5497 0.0 0.0 90.0 3.5497 0.00015 0.0 00000 0170200 2 1020.94 1.0

Component 518

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is used to provide a flow junction from the Volume 18-01 (Component 18) to the Volume 17-01 (Component 17). This component consists of 1 junction (Junction 519). The Junction 519 is corresponding the Connector 19 of the TRANFLO model given in Reference 1.

The smaller of the two flow areas of Volumes 18-01 and 17-01 is 63.49  $ft^2$ which is used as the flow area for this junction. As given the Reference 1, no flow resistance coefficient is specified for the Connector 19. The forward and reverse flow resistant coefficient of 0.0 is used for this The following input are used for the Component 519. junction. sngljun aboverfr 5190000 000000 0.0 0.0 017000000 63.49 018010000 5190101 1.0 1.0 0.0 5190110 0.0 0.0 0.0 0.0 5190201 1

### Component 17 141 1 1/1/96 the 10/2/96

The Component 14 is a single volume with assigned name sgdoom which is used to model the region above the upper deck and below the steam nozzle. This component consists of 1 volume (Volume 17-01). The Volume 17-01 is corresponding the Node 17 of the TRANFLO model given in Reference 1. As given in the Table 4.2.2 of Reference 1, the flow are and volume size for the Node 17 are 94.12 ft<sup>2</sup> and 334.1 ft<sup>3</sup>. The volume length of Node 17 is 334.1/94.12 = 3.5497 ft. The flow area and volume length are specified

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while the volume length is not specified which will be calculated by the code using the volume size and flow area.

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The Volume 18-01 is a horizontal volume. The inclination angle is  $0.0^{\circ}$  and there is no elevation change. The hydraulic diameter of the volume is not specified also and the code will calculate it.

The initial water properties for Node 18 are given in Reference 1 as pressure at 1020.96 psia, temperature at 547°F and void fraction of 1.0 (pure steam). Since there is no superheated steam in the steam generator, the steam in volume 18-01 must be saturated steam. For saturated steam, the RELAP5 code does not allow to specify both the water pressure and temperature. The steam pressure of TRANFLO Node 18 is used for this component. The initial water properties are specified as pressure at 1020.96 psia and the quality of 1.0.

The following input are used for the Component 18. snglvol 0180000 spsteam 00000 0.00015 0.0 0. 0.0 0.0 0.0 473.0 63.49 0180101 1020.96 1.0 0180200 2

#### Component 519

The Component 519 is a single junction with assigned name abovefr which

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for this junction. As given the Reference 1, a forward and reverse flow							
resistant coefficient of 0.5 associated with a flow area of 70.75 $ft^2$ is							
specified for the segment $\frac{1}{2}$ of the Connector 24. If $10/1/96$ f = 10/2/96							
The following input are used for the Component 19.							
	dryer						
<b>019</b> 0001	3	1		0.0	[h	46 10	11/96 fe 10/2/96 015 0.0 00000
0190101	171.4	0.	7083 0.0	0. <b>4</b> <del>0</del> .	0.0	0.00	015 0.0 00000
0190200	2 1	020.9	6 1.0				
<b>019</b> 1101	01901	0000	018000000	63.49	5.502	5.502	000000
0192101	01900	0000	036000000	2.34	0.5	0.5	000000
0193101	02001	0000	019000000	70.75	0.5	0.5	000000
0191201	0.0	0.0	0.0				
0192201	0.0	0.0	0.0				
<b>019</b> 3201	0.0	0.0	0.0				

#### Component 18

The Component 18 is a single volume with assigned name updryer which is used to model the region inside the secondary separator. This component consists of 1 volume (Volume 18-01). The Volume 18-01 is corresponding the Node 18 of the TRANFLO model given in Reference 1. As given in the Table 4.2.2 of Reference 1, the flow are and volume size for the Node 18 are 63.49 ft<sup>2</sup> and 473.0 ft<sup>3</sup>. The volume length of Node 18 is 473.0/63.49 = 7.45 ft. The volume size and flow area are specified as input data

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model. As given in the Reference 1, the smallest flow area of the two segments of the Connector 20 is 63.49 ft<sup>2</sup> which is used as the flow area for this junction. As given the Reference 1, flow resistance is specified for the segments 1 and 2 of the Connector 20, a forward and reverse flow resistant coefficient of 40.0 associated with a flow area of 179.54 ft<sup>2</sup> for segment 1 and a forward and reverse flow resistant coefficient of 0.5 associated with a flow area of 63.49 ft<sup>2</sup> for segment 2. Therefore, for Junction 19-01, the flow resistant coefficient associated with the flow area of 63.49 ft<sup>2</sup> can be calculated as:  $40.0/(179.54/63.49)^2 + 0.5 = 5.002 + 0.5 = 5.502$ 

The Junction 19-02 connects the inlet of Volume 19-01 to the inlet of Volume 36-01 which is corresponding to the Connector 21 of the TRANFLO model. As given in the Reference 1, the smallest flow area of the two segments of the Connector 21 is  $2.34 \text{ ft}^2$  which is used as the flow area for this junction. As given the Reference 1, a forward and reverse flow resistant coefficient of 0.5 associated with a flow area of 2.34 ft<sup>2</sup> is specified for the segment 2 of the Connector 21.

The Junction 19-03 connects the outlet of Volume 20-01 to the inlet of Volume 19-01 which is corresponding to the Connector 24 of the TRANFLO model. As given in the Reference 1, the smallest flow area of the two segments of the Connector 24 is 70.75  $ft^2$  which is used as the flow area

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(Junctions 19-01, 19-02 and 19-03). The Volume 19-01 is corresponding the Node 19 of the TRANFLO model given in Reference 1. As given in the Table 4.2.2 of Reference 1, the flow aregand volume size for the Node 19 are 171.4 ft<sup>2</sup> and 121.4 ft<sup>3</sup>. The volume length of Node 22 is 121.4/171.4= 0.7083 ft. The flow area and volume length are specified as input data while the volume size is not specified which will be calculated by the code using the volume length and flow area.

The Volume 19-01 is a horizontal volume. The inclination angle is  $0^{\circ}$  and there is no elevation change. The hydraulic diameter of the volume is not specified also and the code will calculate it.

The initial water properties for Node 19 are given in Reference 1 as pressure at 1020.96 psia, temperature at 547°F and void fraction of 1.0 (pure steam). Since there is no superheated steam in the steam generator, the steam in volume 19-01 must be saturated steam. For saturated steam, the RELAP5 code does not allow to specify both the water pressure and temperature. The steam pressure of TRANFLO Node 19 is used for this component. The initial water properties are specified as pressure at 1020.96 psia and the quality of 1.0.

The Junction 19-01 connects the outlet of Volume 19-01 to the inlet of Volume 18-01 which is corresponding to the Connector 20 of the TRANFLO

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1-60 is 1.1667 ft and the heat transfer area to the left boundary volumes is 682.9\*1.1667=796.74 ft<sup>2</sup>.

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For Heat Slabs 2, 3, 58 and 59, the length of the left boundary Volumes 1-02, 1-03, 1-58 and 1-59 is 1.2553 ft and the heat transfer area to the left boundary volumes is 682.9\*1.2553=857.24 ft<sup>2</sup>.

For Heat Slabs 4, 5, 8, 9, 12, 13, 16, 17, 20, 21, 24, 25, 28, 29, 32, 33, 36, 37, 40, 41, 44, 45, 48, 49, 52, 53, 56, and 57, the length of the left boundary Volumes 1-04, 1-05, 1-08, 1-09, 1-12, 1-13, 1-16, 1-17, 1-20, 1-21, 1-24, 1-25, 1-28, 1-29, 1-32, 1-33, 1-36, 1-37, 1-40, 1-41, 1-1-44, 1-45, 1-48, 1-49, 1-52, 1-53, 1-56, and 1-57 is 0.5 ft and the heat transfer area to the left boundary volumes is 682.9\*0.5=341.45 ft<sup>2</sup>. For Heat Slabs 6, 7, 10, 11, 14, 15, 18, 19, 22, 23, 26, 27, 34, 35, 38, 39, 42, 43, 46, 47, 50, 51, 54, and 55, the length of the left boundary Volumes 1-06, 1-07, 1-10, 1-11, 1-14, 1-15, 1-18, 1-19, 1-22, 1-23, 1-26, 1-27, 1-34, 1-35, 1-38, 1-39, 1-42, 1-43, 1-46, 1-47, 1-50, 1-51, 1-54, and 1-55 is 1.60435 ft and the heat transfer area to the left boundary volumes is 682.9\*1.60435=1095.61 ft<sup>2</sup>. The length of 3.0 ft is used for Volumes 1-30 and 1-31. As described in the section for Component 1, the actual tube length modeled in the Volumes 1-30 and 1-31 is 3.2075 ft. Therefore, for the heat slabs 30 and 31, the heat transfer area to the left boundary Volumes 1-30 and 1-31 is  $682.9 \times 3.2075 = 2190.4 \text{ ft}^2$ .

For each heat slab, the right boundary volume has the same length as the

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left boundary volume. Since the tubes have cylindrical shape, the ratio of the heat transfer areas for the right and left boundary volumes for all heat slabs equals to the ratio of the outside diameter and inside diameter of the tubes. The outside diameter of the tubes is the sum of the inside diameter of the tubes and twice of the tube wall thickness which can be calculated as 0.0642 + 2\*0.00438 = 0.07296 ft. The ratio of the heat transfer areas for the right and left boundary volumes for all heat slabs equals to 0.07296/0.0642 = 1.136449. Then, the heat transfer area of the right boundary volume for each heat slab can be calculated as the heat transfer area of the left boundary volume for heat slab multiplied by 1.136449.

For Heat Slabs 1 and 60, the heat transfer area to the right boundary volumes is 1.136449\*796.74 =905.4541 ft<sup>2</sup>. For Heat Slabs 2, 3, 58 and 59, the heat transfer area to the right boundary volumes is 1.136449\*857.24=974.2092 ft<sup>2</sup>. For Heat Slabs 4, 5, 8, 9, 12, 13, 16, 17, 20, 21, 24, 25, 28, 29, 32, 33, 36, 37, 40, 41, 44, 45, 48, 49, 52, 53, 56, and 57, the heat transfer area to the right boundary volumes is 1.136449\*341.45=388.0404 ft<sup>2</sup>. For Heat Slabs 6, 7, 10, 11, 14, 15, 18, 19, 22, 23, 26, 27, 34, 35, 38, 39, 42, 43, 46, 47, 50, 51, 54, and 55, the heat transfer area to the right boundary volumes is 1.136449\*1095.61=1245.1044 ft<sup>2</sup>. For Heat Slabs 30 and 31, the heat transfer area to the right boundary volumes is

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1.136449\*2190.4=2489.277 ft<sup>2</sup>.

There is no heat source in all heat slabs. The initial source multiplier and the direct moderator heating multipliers for both left and right boundary volumes are set to be 0.0. The hydraulic diameters for all the left and right boundary volumes are used for the heat transfer hydraulic diameter. Since the heat transfer rate through the tubes is much lower than the CHF, arbitrary large values or default values are used for all the input related to CHF calculation for both the left and right boundary volumes.

The input data for the heat slabs are listed as follows.

11201000	60	11	2	1	0.03	21	-	
11201100	0	2						
11201101	0.00	0438	10	)				
11201201	1	10						
11201301	0.0	10						
11201401	547.	0 1	1					
11201501	0010	10000		0000	1	0	796.74	1
11201502	0010	20000	]	0000	1	0	857.24	3
11201503	0010	40000	]	0000	1	0	341.45	5
11201504	0010	60000	]	0000	1	0	1095.61	7
11201505	0010	00008	]	0000	1	0	341.45	9

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11201506	001100000	10000	1	0	1095.61	11
11201507	001120000	10000	1	0	341.45	13
11201508	001140000	10000	1	0	1095.61	15
11201509	001160000	10000	1	0	341.45	17
11201510	001180000	10000	1	0	1095.61	19
11201511	001200000	10000	1	0	341.45	21
11201512	001220000	10000	1	0	1095.61	23
11201513	001240000	10000	1	0	341.45	25
11201514	001260000	10000	1	0	1095.61	27
11201515	001280000	10000	1	0	341.45	29
11201516	001300000	10000	1	0	2190.4	31
11201517	001320000	10000	1	0	341.45	33
11201518	001340000	10000	1	0	1095.61	35
11201519	001360000	10000	1	0	341.45	37
11201520	001380000	10000	1	0	1095.61	39
11201521	001400000	10000	1	0	341.45	41
11201522	001420000	10000	1	0	1095.61	43
11201523	001440000	10000	1	0	341.45	45
11201524	001460000	10000	1	0	1095.61	47
11201525	001480000	10000	1	0	341.45	49
11201526	001500000	10000	1	0	1095.61	51
11201527	001520000	10000	1	0	341.45	53
11201528	001540000	10000	1	0	1095.61	55

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11201529	001560000	10000	1	0	341.45	57
11201530	001580000	10000	1	0	857.24	59
11201531	001600000	0000	1	0	796.74	60
11201601	030010000	0000	1	0	905.4541	1
11201602	002010000	10000	1	0	974.2092	3
11201603	002030000	10000	1	0	388.0404	5
11201604	002050000	10000	1	0	1245.1044	7
11201605	002070000	10000	1	0	388.0404	9
11201606	002090000	10000	1	0	1245.1044	11
11201607	002110000	10000	1	0	388.0404	13
11201608	002130000	10000	1	0	1245.1044	15
11201609	002150000	10000	1	0	388.0404	17
11201610	002170000	10000	1	0	1245.1044	19
11201611	002190000	10000	1	0	388.0404	21
11201612	002210000	10000	1	0	1245.1044	23
11201613	002230000	10000	1	0	388.0404	25
11201614	002250000	10000	1	0	1245.1044	27
11201615	002270000	10000	1	0	388.0404	29
11201616	002290000	0000	1	0	2489.277	31
11201617	002280000	-10000	1	0	388.0404	33
11201618	002260000	-10000	1	0	1245.1044	35
11201619	002240000	-10000	1	0	388.0404	37
11201620	002220000	-10000	1	0	1245.1044	39

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11201621	002200000 -10000	1 0	388.0404	41		
11201622	002180000 -10000	1 0	1245.1044	43		
11201623	002160000 -10000	1 0	388.0404	45		
11201624	002140000 -10000	1 0	1245.1044	47		
11201625	002120000 -10000	1 0	388.0404	49		
11201626	002100000 -10000	1 0	1245.1044	51		
11201627	002080000 -10000	1 0	388.0404	53		
11201628	002060000 -10000	1 0	1245.1044	55		
11201629	002040000 -10000	1 0	388.0404	57		
11201630	002020000 -10000	1 0	974.2092	59		
11201631	003010000 0000	1 0	905.4541	60		
11201701	0 0.0 0.0 0.0	60				
11201801	0.0 15.0 15.0	1.5	1.5 0.0	0.0	1.0	60
11201901	0.0 15.0 15.0	1.5	1.5 0.0	0.0	1.0	60
20100100	tbl/fctn 1 1					
20100101	70.0	2.3843	3e-03			
	•					

20100102	200.0	2.5232e-03
20100103	400.0	2.8009e-03
20100104	600.0	3.0787e-03
20100105	800.0	3.3565e-03
20100106	1000.0	3.6574e-03
20100107	1200.0	3.9815e-03

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20100108	1400.0	<b>4.3056e-03</b>
20100151	70.0	55.6831
20100152	200.0	55.5227
20100153	400.0	55.2607
20100154	600.0	54.9895
20100155	800.0	54.7069
20100156	1000.0	54.3982
20100157	1200.0	54.0907
20100158	1400.0	53.7516

#### Control Variables

The purpose of this analysis is to determine the pressure difference across the TSPs. In this calculation, the pressure difference across the TSP is defined as the pressure at the center of the volume immediately above the TSP subtracting the pressure at the center of the volume immediately below the TSP. Since the length of the volume immediately above or below the TSP is 0.5 ft, this definition conservatively adds a 0.5 ft hydraulic head to the actual pressure difference across TSP. Control Variables 1 to 7 are used to calculate the differential pressures across TSPs 1 to 7.

#### Control Variable 1

### CALC NO. STA-042 <u>Ro</u> SUBJECT <u>Loads on the Steam Generator Support Plats During SLB Accident</u> MADE BY <u>H M Lee</u> DATE <u>10/1/96</u> CHECK BY <u>L R Chang</u> APPROVED BY

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Control Variable 1 is named as delptp1 which is used to calculate the differential pressure across TSP 1. The delptp1 is the sum of the negative pressure of the Volume 2-04 and the pressure of the Volume 2-03. The RELAP5 code used pa for the pressure. As given in Reference 3, a pa equals to 1.45038e-4 psi. A conversion factor of 1.45038e-4 is used in the Control Variable 1. The following input is used for the Control Variable 1.

20500100 delptpl sum 1.45038e-4 0.0 l 20500101 0.0 -1.0, p, 002040000 1.0, p, 002030000

#### Control Variable 2

Control Variable 2 is named as delptp2 which is used to calculate the differential pressure across TSP 2. The delptp2 is the sum of the negative pressure of the Volume 2-08 and the pressure of the Volume 2-07. A conversion factor of 1.45038e-4 is used in the Control Variable 2 to convert pa to psi. The following input is used for the Control Variable 2.

20500200delptp2sum1.45038e-40.01205002010.0-1.0,p,0020800001.0,p,002070000

#### Control Variable 3

Control Variable 3 is named as delptp3 which is used to calculate the differential pressure across TSP 3. The delptp3 is the sum of the

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negative pressure of the Volume 2-12 and the pressure of the Volume 2-11. A conversion factor of 1.45038e-4 is used in the Control Variable 3 to convert pa to psi. The following input is used for the Control Variable 3.

20500300 delptp3 sum 1.45038e-4 0.0 1 20500301 0.0 -1.0, p, 002120000 1.0, p, 002110000

#### Control Variable 4

Control Variable 4 is named as delptp4 which is used to calculate the differential pressure across TSP 4. The delptp4 is the sum of the negative pressure of the Volume 2-16 and the pressure of the Volume 2-15. A conversion factor of 1.45038e-4 is used in the Control Variable 4 to convert pa to psi. The following input is used for the Control Variable 4.

20500400 delptp4 sum 1.45038e-4 0.0 1 20500401 0.0 -1.0, p, 002160000 1.0, p, 002150000

#### Control Variable 5

Control Variable 5 is named as delptp5 which is used to calculate the differential pressure across TSP 5. The delptp5 is the sum of the negative pressure of the Volume 2-20 and the pressure of the Volume 2-19. A conversion factor of 1.45038e-4 is used in the Control Variable 5 to convert pa to psi. The following input is used for the Control Variable

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5.

20500500 delptp5 sum 1.45038e-4 0.0 l 20500501 0.0 -1.0, p, 002200000 1.0, p, 002190000

#### Control Variable 6

Control Variable 6 is named as delptp6 which is used to calculate the differential pressure across TSP 6. The delptp6 is the sum of the negative pressure of the Volume 2-24 and the pressure of the Volume 2-23. A conversion factor of 1.45038e-4 is used in the Control Variable 6 to convert pa to psi. The following input is used for the Control Variable 6.

20500600 delptp6 sum 1.45038e-4 0.0 l 20500601 0.0 -1.0, p, 002240000 l.0, p, 002230000

#### Control Variable 7

Control Variable 7 is named as delptp7 which is used to calculate the differential pressure across TSP 7. The delptp7 is the sum of the negative pressure of the Volume 2-28 and the pressure of the Volume 2-27. A conversion factor of 1.45038e-4 is used in the Control Variable 7 to convert pa to psi. The following input is used for the Control Variable 7.

20500700 delptp7 sum 1.45038e-4 0.0 l 20500701 0.0 -1.0, p, 002280000 l.0, p, 002270000

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#### Time Step Control

A very small minimum time step of  $1.0e^{-7}$  second is used for the entire run to insure that the time step can be reduced to the required size as determined by the RELAP5 time step control scheme. The steam line break is occurred at 5 seconds for this analysis. For the first 5 seconds, the steam generator is in steady state condition. The purpose for the first 5 seconds run is to self correct the slightly inconsistence in the input and a real steady state condition can be provided at the initiation of the break. For steady state run, larger time steps can be used. A maximum time step of 0.005 second is used for the first 5 seconds run.

After the initiation of the break, a very large steam flow is blown out from the steam generator which induces a very fast transient in the steam generator. In addition, a great portion of the water in the steam generator is in pure liquid phase at the initiation of the break. The depressurization wave travels at a very high speed in the liquid water. To correctly track the depressurization wave front and to limit the water property change in the components during each time step, a maximum time step of 1.0e<sup>-5</sup> second is used immediately after the initiation of break. The depressurization wave travelling speed is substantially reduced when flashing occurs in the liquid region due to depressurization. Then, the maximum time step size can be increased. A maximum time step size of 2.5e<sup>-5</sup> second is used starting at 0.3 second after the initiation of the

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break (5.3 seconds into the run). The maximum time step size is further increased to  $5e^{-5}$  second starting at 1.5 seconds after the initiation of the break (6.5 seconds into the run). The analysis is terminated at 3 seconds after the initiation of the break (8 seconds into the run). A maximum time step size of  $1.0e^{-4}$  second is specified in the input after 8 seconds which is not used in the run.

During the entire run, the standard major edits are printed. The time step control options ss and d are set to 0. The time step control option tt is set to 3 which allows to use a mass error analysis to control the hydrodynamics advancement time step size in addition to standard time step control. The heat conduction/transfer time step is set to the same as the hydrodynamics time step. Since the maximum time step sizes allowed are very small, the maximum time step sizes are used during the entire run. Therefore, the time step control option has no effect on the analysis.

The minor edits are printed out every 0.1 seconds which is the frequency of the differential pressure used in the TSP structure analysis performed by Westinghouse. Due to 109000 time steps advanced during the run, the major edit frequency is set to be very small to reduce the output to a manageable size. The restart is not used. An arbitrary small restart frequency is used.

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The following input is used for the time step control.

201	5.0	1.d-7	0.005	3	2	200	10000
202	5.3	1.d-7	0.00001	3	1000	20000	100000
203	6.5	1.d-7	0.000025	3	400	8000	100000
204	8.0	1.d-7	0.00005	3	200	10000	100000
205	1000.0	1.d-7	0.0001	3	100	10000	100000

#### <u>Trip Cards</u>

Three trip cards are used in the input. The Trip Card 501 is used to terminate the analysis at 8 seconds. The Trip Card 502 is used to initiate the steam line break at 5 seconds. The Trip Card 503 is used to close the steam line break at an arbitrary large time of 200 seconds. For all the three Trip Cards, the latch indicator is set to 1 which makes all the three trips once set true remain true. The following input is used for the Trip Cards.

501	time	0	ge	null	0	8.0	1	
502	time	0	ge	null	0	5.0	٦	
503	time	0	ge	null	0	200.0	1	

#### Trip Stop Advancement Card

The Trip Card 501 is used to terminate the analysis. The following input is used for the trip stop advancement card. 600 501

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#### Miscellaneous Input

The following input is used to indicate the problem type is a new transient.

```
100 new transnt
```

The following input is used to select the british units for both input and out output.

102 british british

To tern off the CPU time check and diagnostic edit, empty Card 105 is input.

#### 105

The following variables are listed in the minor edit.

The flow rates at TSPs (Junctions 2-03, 2-07, 2-11, 2-15, 2-19, 2-23 and 2-27) and the break (Junction 518).

- The pressure at the volume upstream the break (Volume 17-01).
- The differential pressures across the TSPs (Control Variables 1 to 7).

The following input is used to select the minor edit.

301 mflowj 518000000

302 mflowj 002030000

mflowj

303

# SHEET NO. $\frac{\$ \Psi}{\text{STA-042}} = \frac{\$ \Psi}{\cancel{R} o}$

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002070000

- 320 cntrlvar 2
- 321 cntrlvar 3 322 cntrlvar 4
- 323 cntrlvar 5 324 cntrlvar 6
- 326 cntrlvar 7

The title of the analysis is set as follows. =SLB pressure difference across the SG tube support plates The input file name is reidpl and the output file name is reodpl.

The complete list of the input is attached in the Appendix D.

#### RELAP5 Input for LB Case 2

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The only difference between the LB Case 1 and LB Case 2 is the equilibrium model is used in LB Case 2 for the volumes modeling the shell side of the steam generator tubes. Therefore, the only input changes from LB Case 1 to LB Case 2 are the volume control flag e is set to 1 for Volumes 2-01 to 2-30. The following input changes are used for LB Case 2.

0021001 00101 29

0021002 00001 30

The remaining input are the same as those for the LB Case 1. The input file name is reidp2 and the output file name is reodp2.

#### RELAP5 Input for LB Case 3

The only difference between the LB Case 1 and LB Case 3 is the initial steam generator water level and flow resistance of the TSPs. The initial water level used in LB Case 1 is 490.5" above the steam generator tube plate, while the initial water level used in LB Case 3 is 466.0" above the steam generator tube plate. The initial void fractions for the Volumes 23-01, 32-01, 33-01 and 36-01 are changed to 0.39, 1.0, 0.93 and 1.0 from those used for the LB Case 1, as shown in Appendix C for case 61. As discussed for LB Case 1 input, the void fractions are conservatively used as qualities for LB Case 3. The initial pressures at each of the Volumes are slightly reduced due to lower water level. However, since five seconds steady state run is performed before the

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initiation of the break, the volume pressures will be self-corrected when the break is initiated. Therefore, it is not necessary to change the initial volume pressures for this case. The flow resistant coefficient of 0.78 is used for forward and reverse flow through the TSPs for LB Case 1. For LB Case 3, the flow resistant coefficient is increased to 0.99 for forward and reverse flow through the TSPs. The following input changes are used for LB Case 3.

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STA-042 KD

CALC NO.

- 0230200 2 1022.72 0.39
- 1.0 0320200 2 1021.26 0.93 0330200 2 1021.72 1021.57 0.82 2 0360200 0.99 0.99 0020902 3 0020904 0.99 0.99 7
- 0020906 0.99 0.99 11
- 0020908 0.99 0.99 15
- 0020910 0.99 0.99 19
- 0020912 0.99 0.99 23
- 0020914 0.99 0.99 27

The remaining input are the same as those for the LB Case 1.

The input file name is reidp5 and the output file name is reodp5.

#### RELAP5 Input for SB Case 1

The only difference between the LB Case 1 and SB Case 1 is the steam line

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break size. For LB Case 1, the cross section area of the steam generator steam outlet nozzle is used for the break size. For SB Case 1, the cross section area of the steam pipe down stream the flow restrictor is used. As given in Reference 1, the break size of 1.388  $ft^2$  is used for the SB Case 1. Therefore, the only input change from LB Case 1 to SB Case 1 is that the flow area of Junction 518 is changed from 4.6  $ft^2$  to 1.388  $ft^2$ . The following input change is used for SB Case 1 0.0 0.0 000100 038000000 1.388 5180101 017010000 The remaining input are the same as those for the LB Case 1. The input file name is reidp3 and the output file name is reodp3.

#### RELAP5 Input for SB Case 2

The only difference between the SB Case 1 and SB Case 2 is the equilibrium model is used in SB Case 2 for the volumes modeling the shell side of the steam generator tubes. Therefore, the only input changes from SB Case 1 to SB Case 2 are the volume control flag e is set to 1 for Volumes 2-01 to 2-30. The following input changes are used for SB Case 2.

0021001 00101 29

0021002 00001 30

The remaining input are the same as those for the SB Case 1. The input file name is reidp4 and the output file name is reodp4.

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#### 6. Results

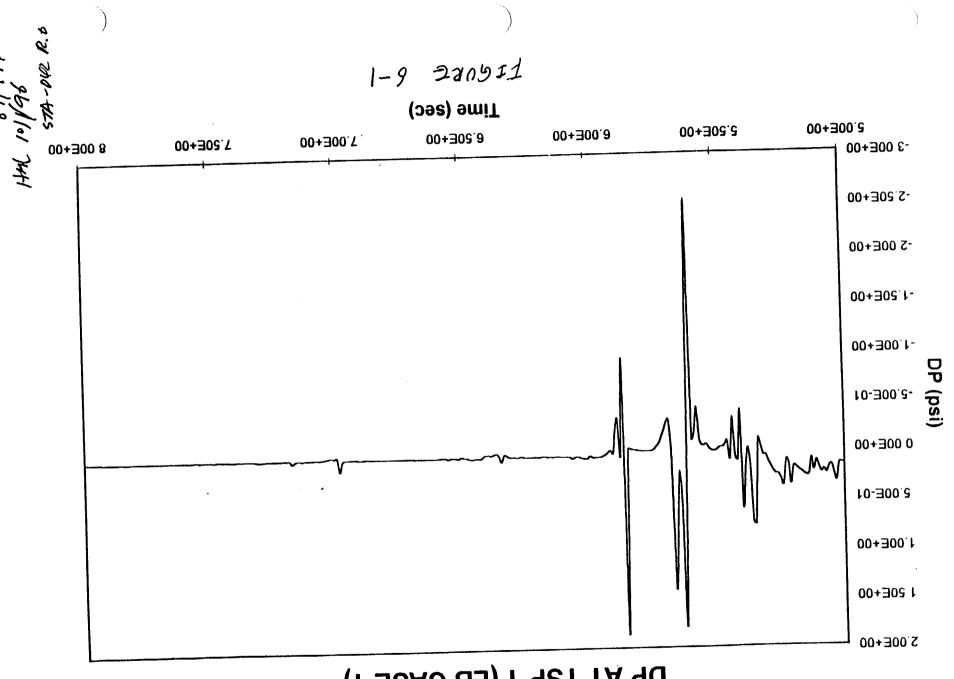
The results of all RELAP5 runs are microfiched and attached to the calculation file as Appendix G.

#### Large Break Case 1

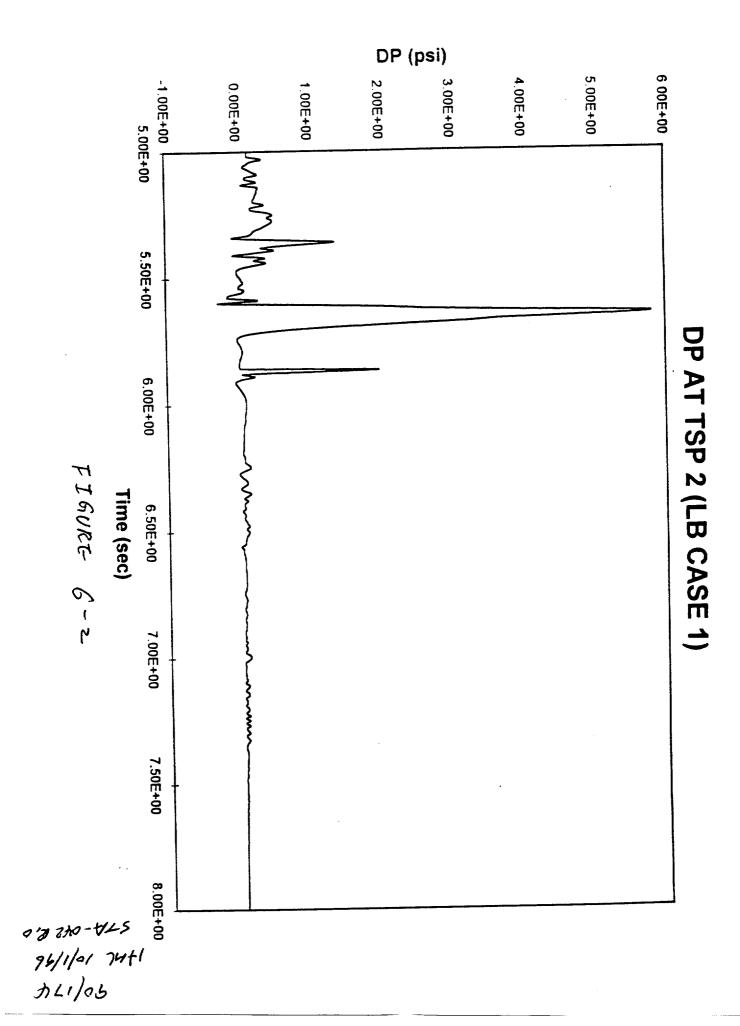
The time history of the differential pressures across TSPs 1 to 7 after the initiation of the break are plotted on Figures 6-1 to 6-7. The peak differential pressures across the TSPs 1 to 7 are 1.855 psi, 5.774 psi, 9.489 psi, 9.732 psi, 9.541 psi, 9.411 and 8.784 psi, respectively. All the peak pressures are occurred at 0.5 to 0.8 second after the initiation of the break. The duration of the high differential pressure across the TSP is very short for the TSP 1 which is located nearest to the bottom of the steam generator. The duration increases when the location of the TSP is further away from the bottom of the steam generator. Therefore, even the difference is very small between the peak differential pressures across the TSPs 3 to 7, the integrated force acting on the TSP increases with the elevation of the TSP.

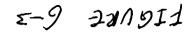
#### Large Break Case 2

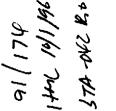
The time history of the differential pressures across TSPs 1 to 7 after the initiation of the break are plotted on Figures 6-8 to 6-14. The peak differential pressures across the TSPs 1 to 7 are 1.938 psi, 2.17

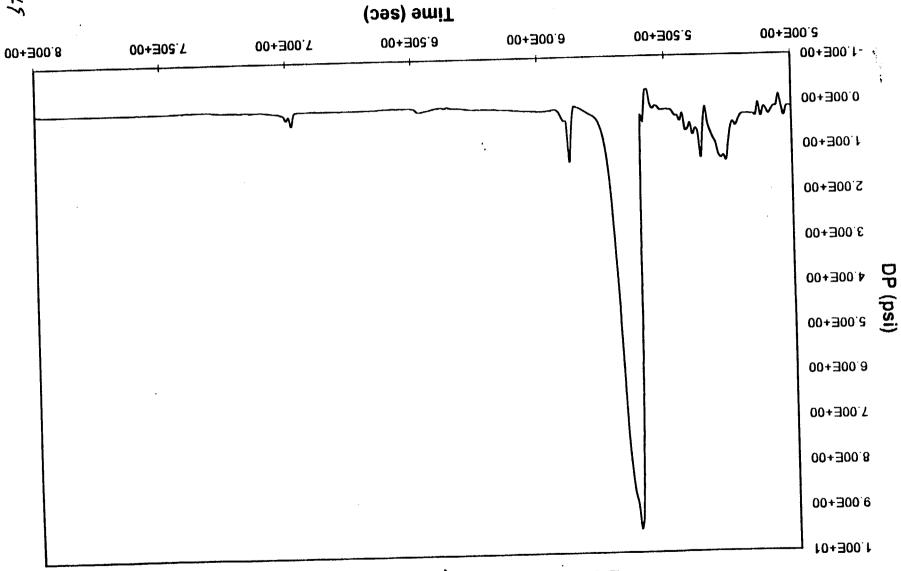


# DP AT TSP 1 (LB CASE 1)

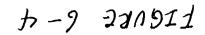




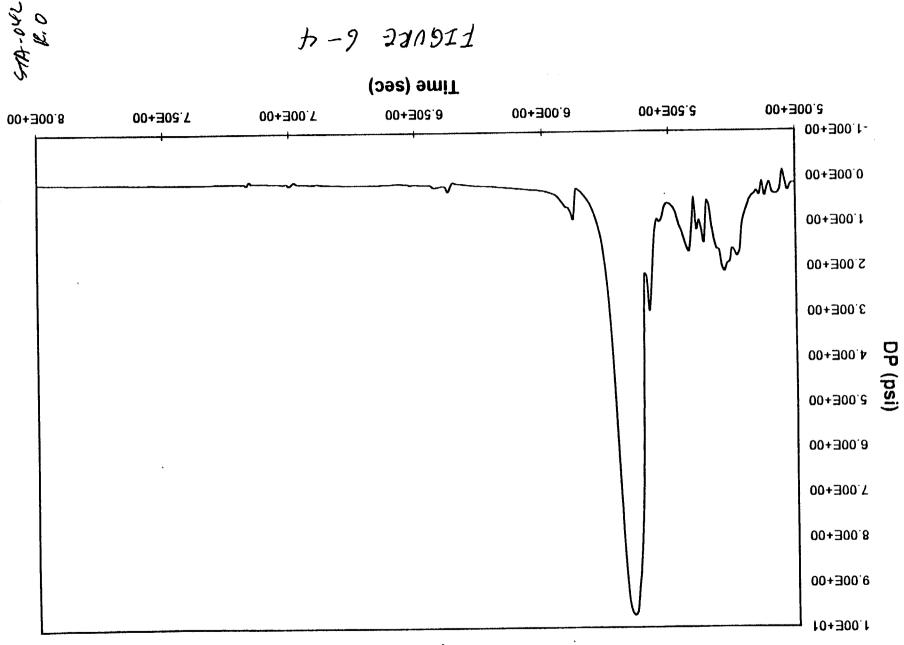




# DP AT TSP 3 (LB CASE 1)

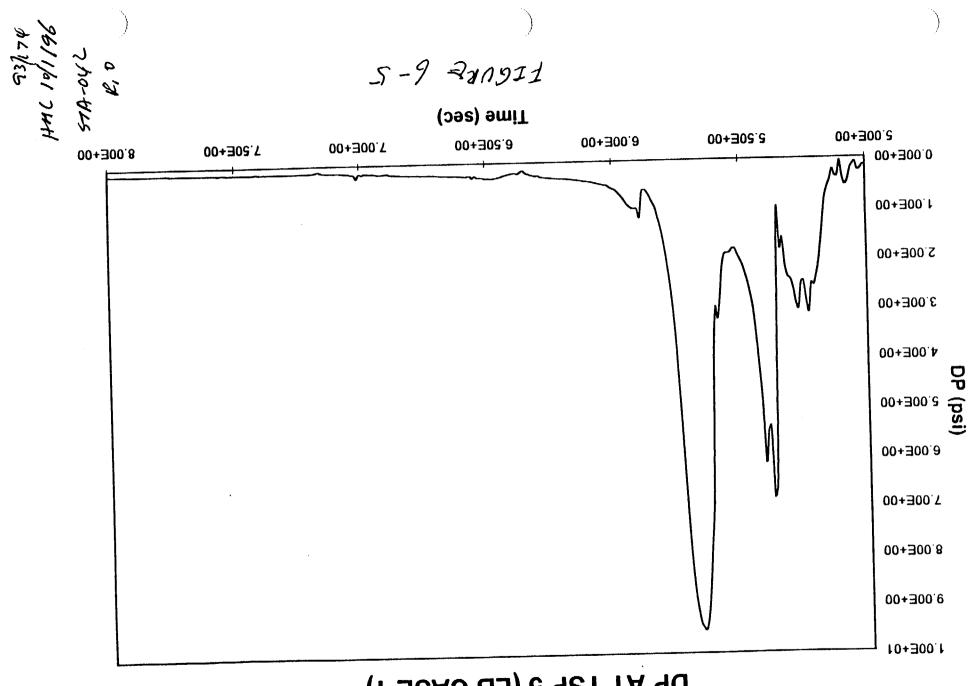


16/1/01 24/1 25/125



## DP AT TSP 4 (LB CASE 1)

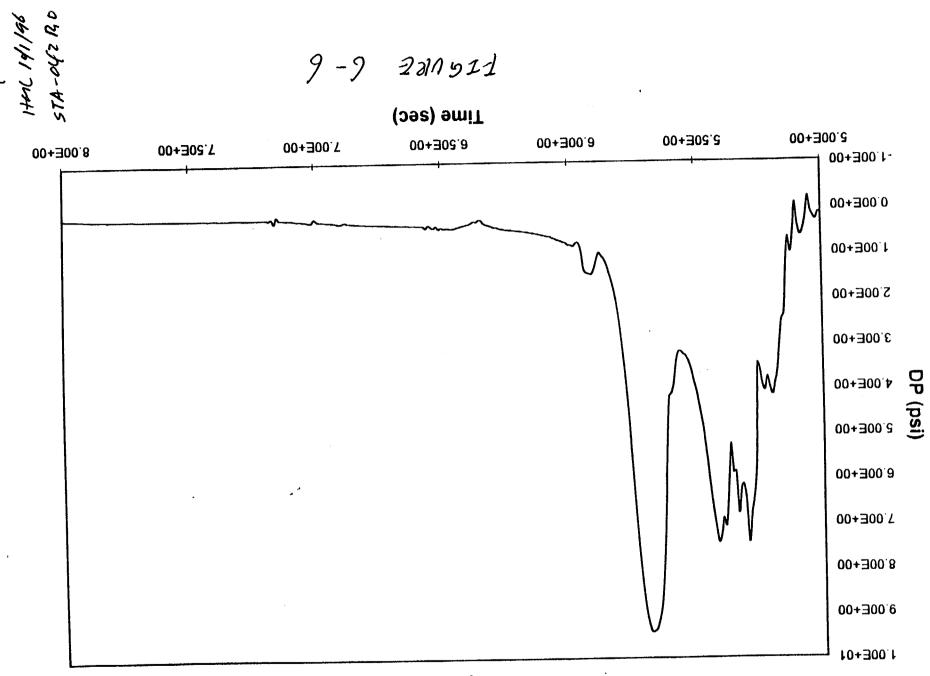
 $\left\{ \right\}_{i}$ 



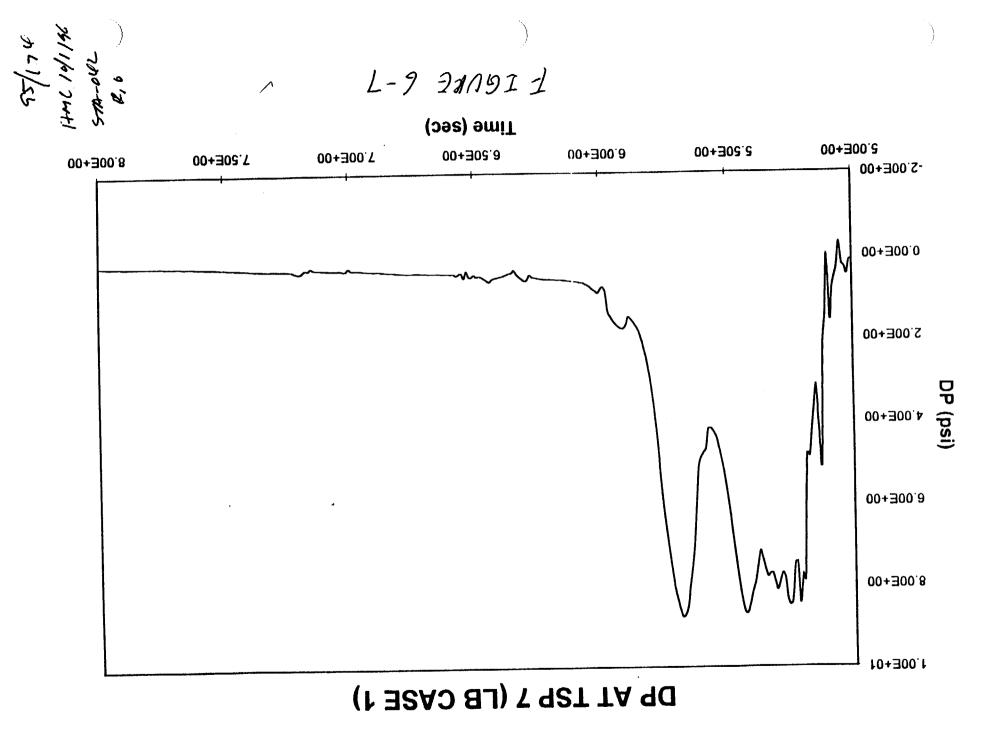
# DP AT TSP 5 (LB CASE 1)

9-9 2211921

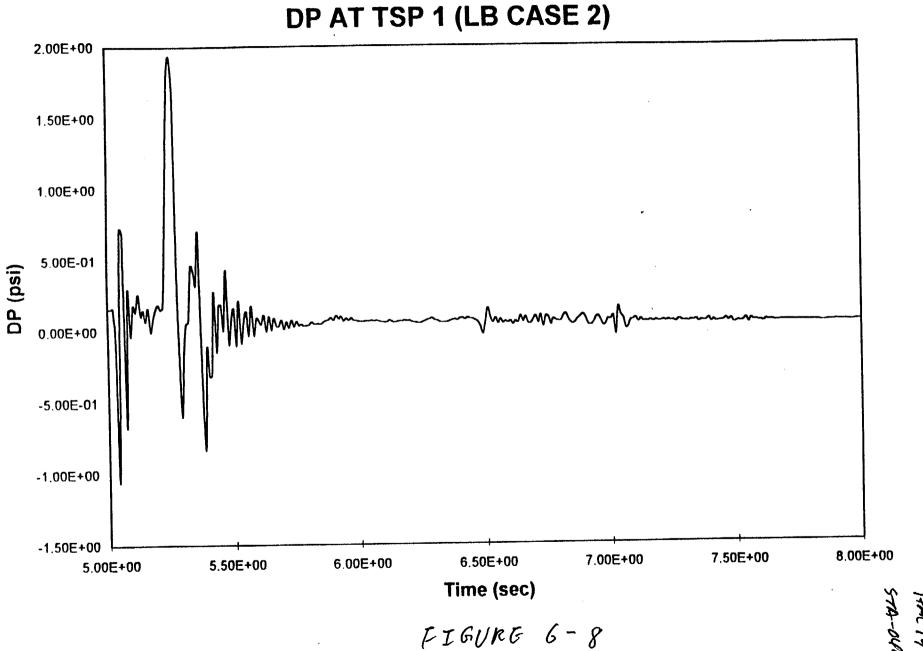
94/174

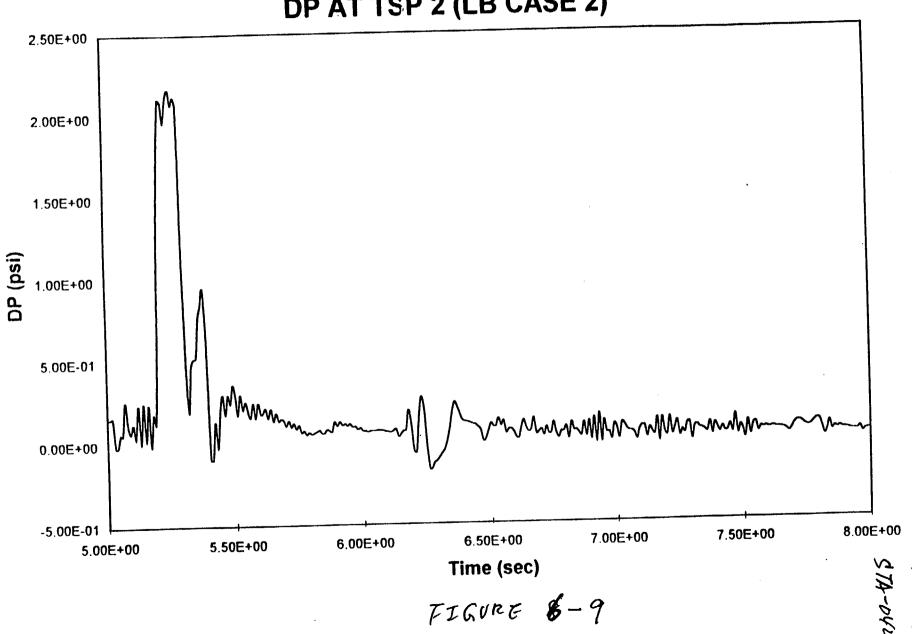


### DP AT TSP 6 (LB CASE 1)

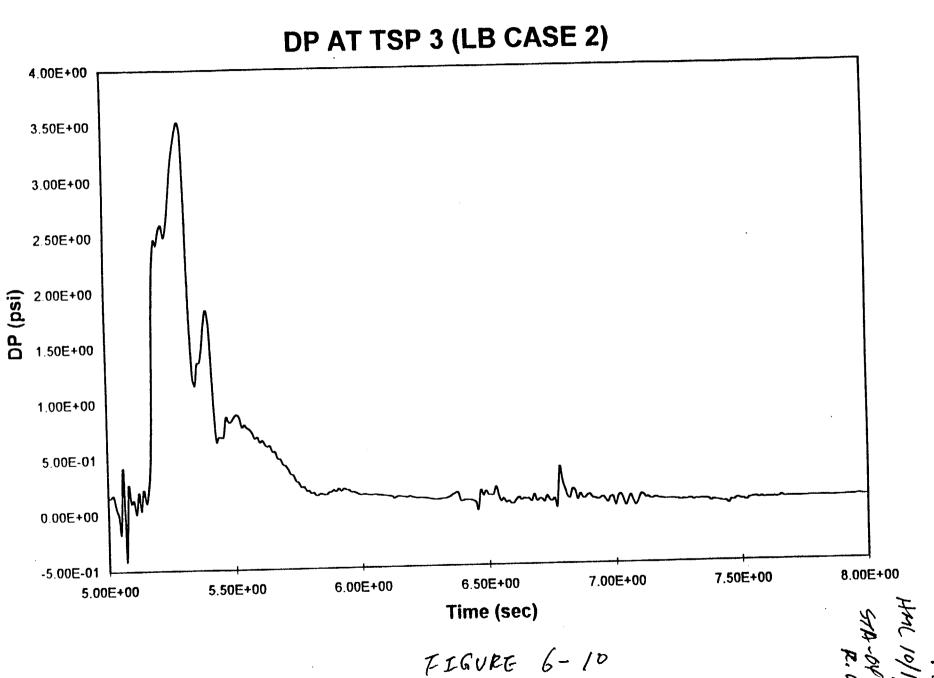


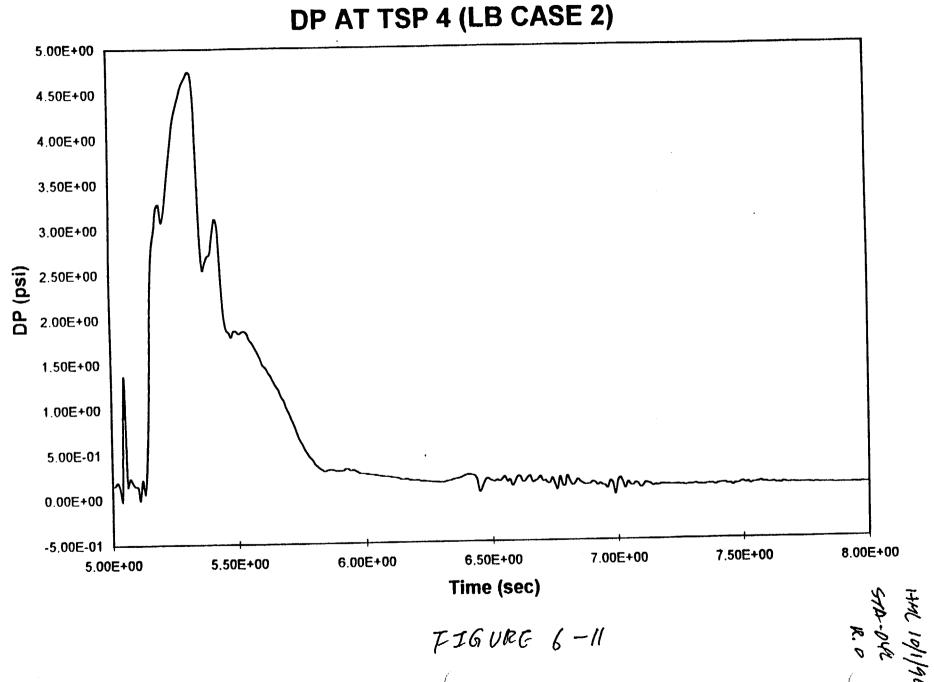
...\*

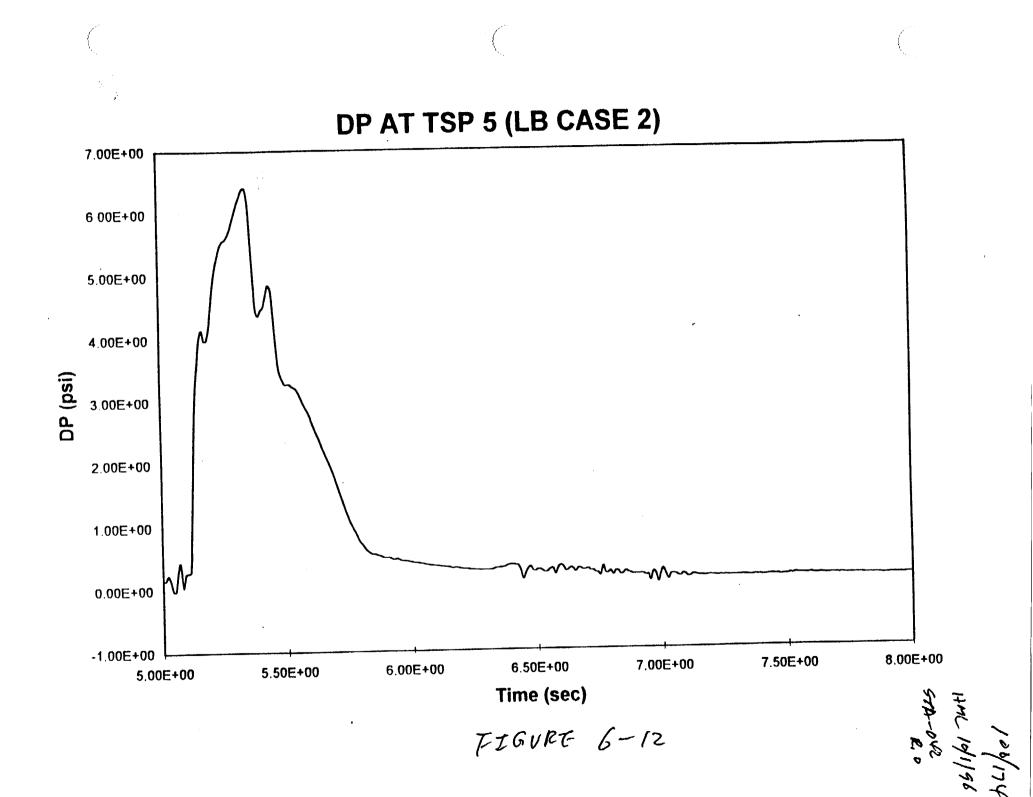


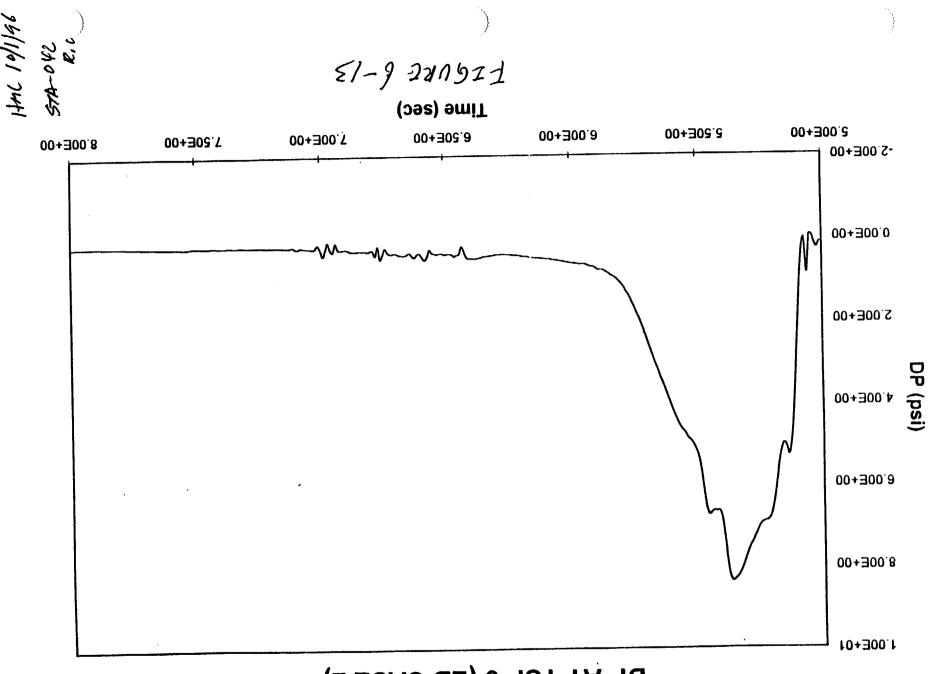


# DP AT TSP 2 (LB CASE 2)





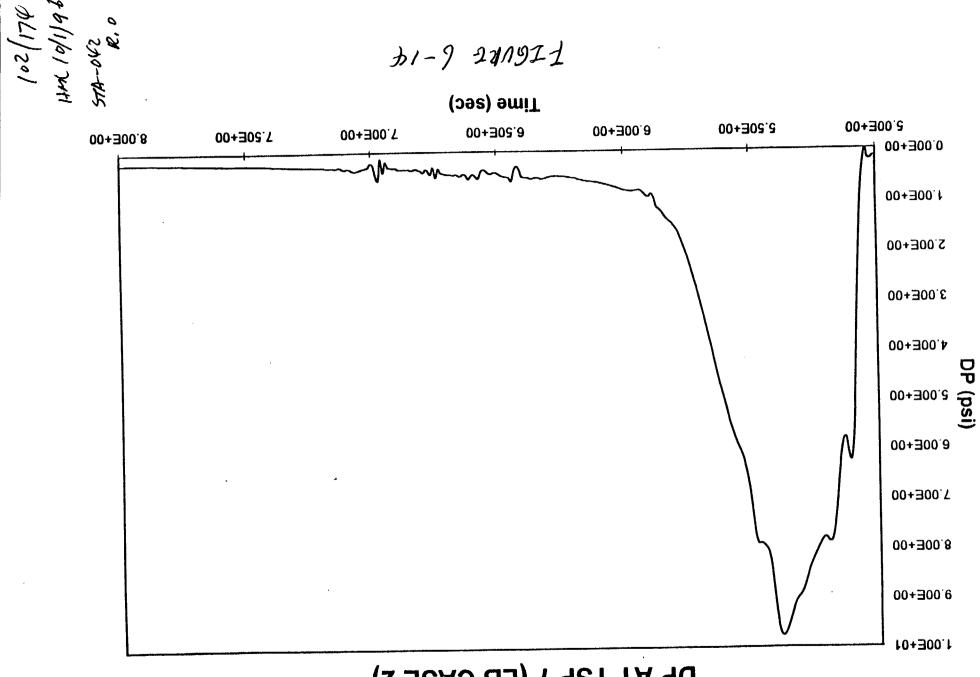




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### DP AT TSP 6 (LB CASE 2)

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# DP AT TSP 7 (LB CASE 2)

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psi, 3.534 psi, 4.751 psi, 6.418 psi, 8.376 and 9.769 psi, respectively. The peak pressure across the TSP increases substantially with the increase of the TSP elevation for LB Case 2 which is quite different from the LB Case 1. All the peak pressures are occurred at 0.3 to 0.5 second after the initiation of the break which is also much earlier than those for LB Case 1. In addition, more smooth time histories are noticed for the differential pressures acting on the TSPs for LB Case 2. Similar to LB Case 1, the duration of the high differential pressure across the TSP is very short for the TSP 1 which is located nearest to the bottom of the steam generator. The duration increases when the location of the TSP is further away from the bottom of the steam generator. Except for TSPs 1 and 7, the peak differential pressures at TSPs 2 to 6 for LB Case 2 are substantially lower than those for LB Case 1. However, in general, the duration of the high differential pressure acting on each TSP is longer for LB Case 2 than that for LB Case 1. Therefore, the difference between the integrated forces acting on the TSPs for LB Case 1 and LB Case 2 are not substantial.

As discussed above, the characteristic of the differential pressures across the TSPs for LB Case 2 is substantially different from that for LB Case 1 which is a result of changing the modeling scheme from nonequilibrium to equilibrium for the shell side of the tube region. Since this is a very fast transient, it is difficult to determine which case is

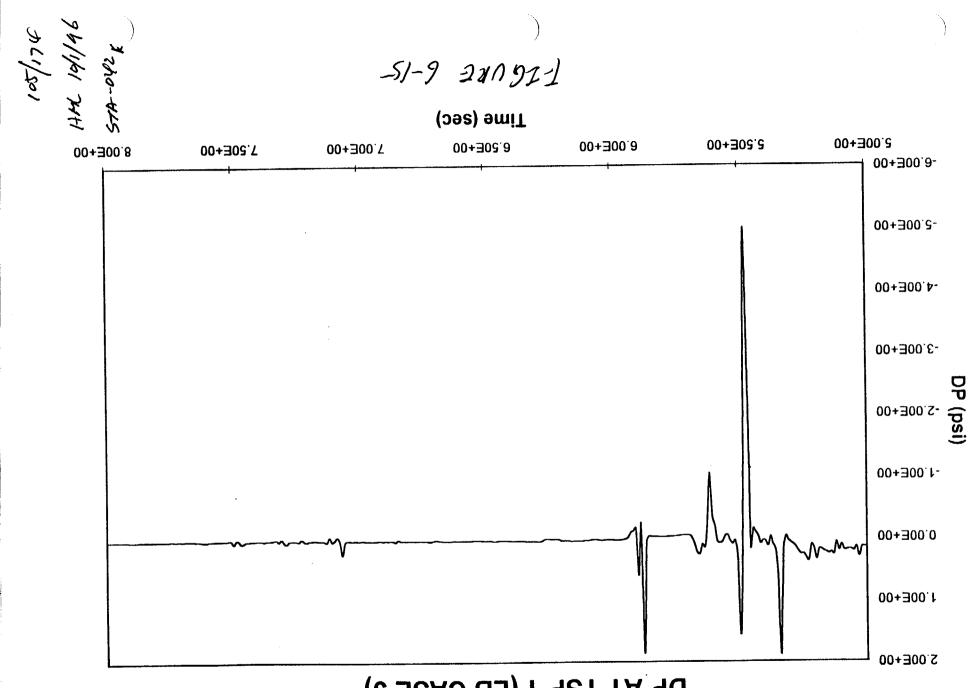
more accurate. Therefore, the results of both cases are transmitted to Westinghouse to perform structure analysis for the TSPs.

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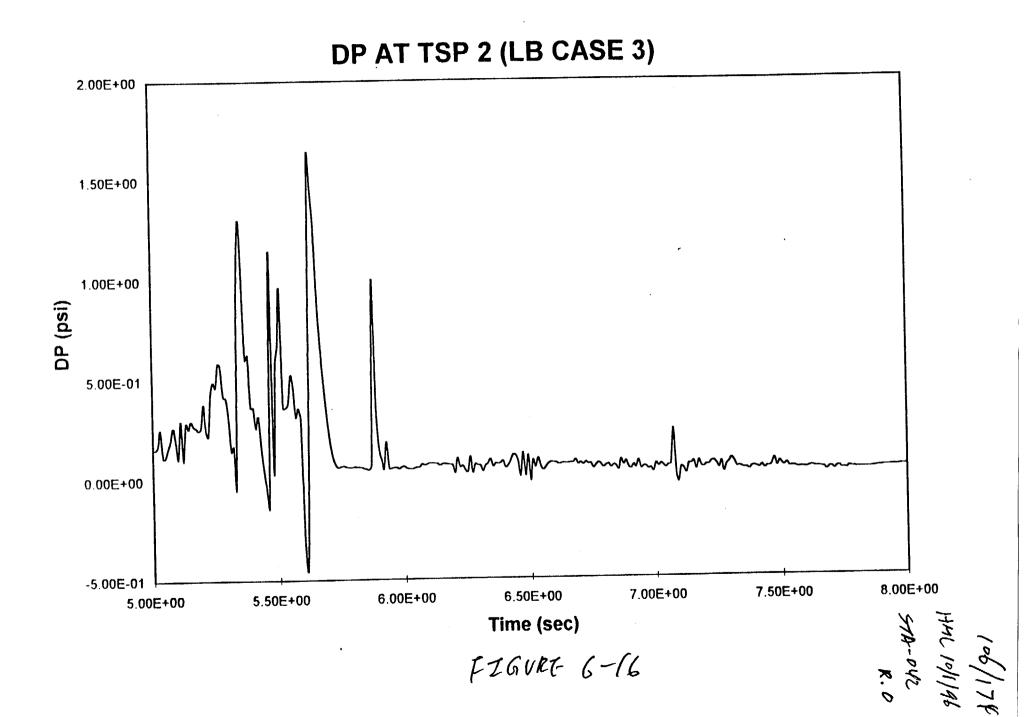
#### Large Break Case 3

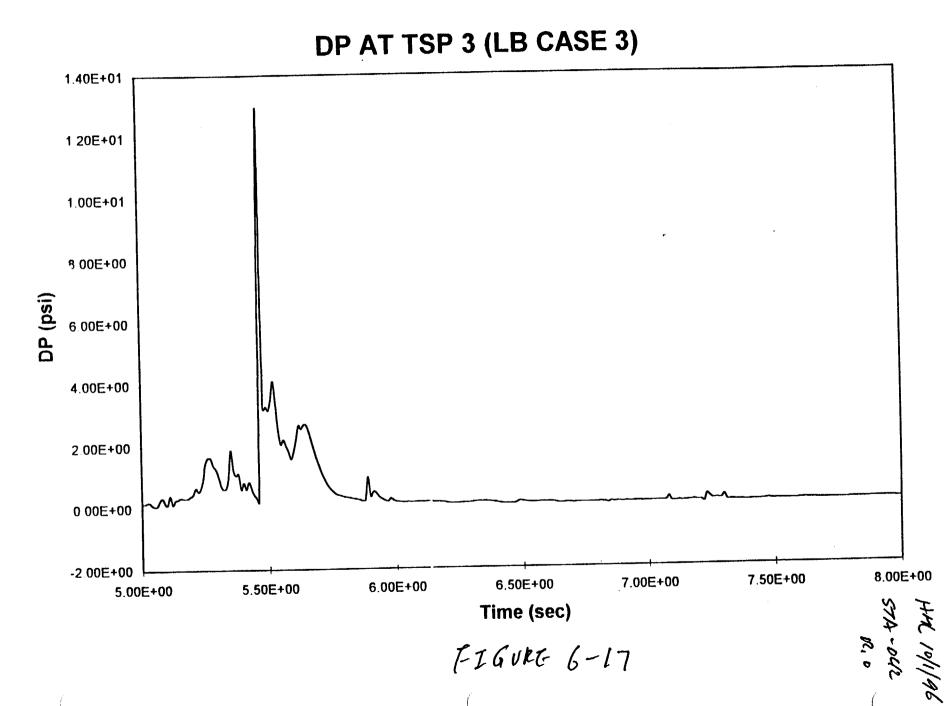
The time history of the differential pressures across TSPs 1 to 7 after the initiation of the break are plotted on Figures 6-15 to 6-21. The peak differential pressures across the TSPs 1 to 7 are -4.915 psi, 12.93 psi, 12.93 psi, 11.24 psi, 10.98 psi, 11.57 and 12.84 psi, respectively. As shown in Figure 6-15 and 6-17, the peak differential pressure across TSPs 1 and 3 for LB Case 3 are spikes with very short duration which can not be explained physically. Excluding the spikes, the peak differential pressures across the TSPs 1 and 3 are 1.885 psi and 4.106 psi, respectively. All the peak pressures are occurred at 0.4 to 0.6 second after the initiation of the break which is earlier than those for LB Case 1. Similar the LB Case 1, the duration of the high differential pressure across the TSP is very short for the TSP 1 which is located nearest to the bottom of the steam generator. The duration increases when the location of the TSP is further away from the bottom of the steam generator. Therefore, even the difference is very small between the peak differential pressures across the TSPs 4 to 7, the integrated force acting on the TSP increases with the elevation of the TSP.

Comparison between the differential pressures across the TSPs for LB Case

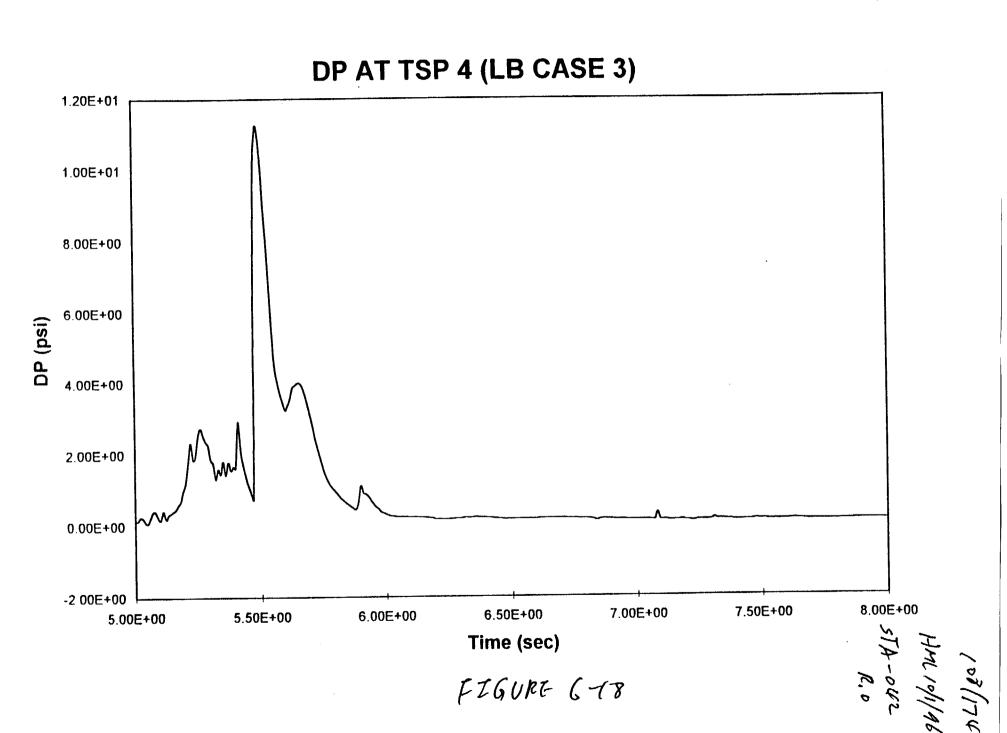


## DP AT TSP 1 (LB CASE 3)

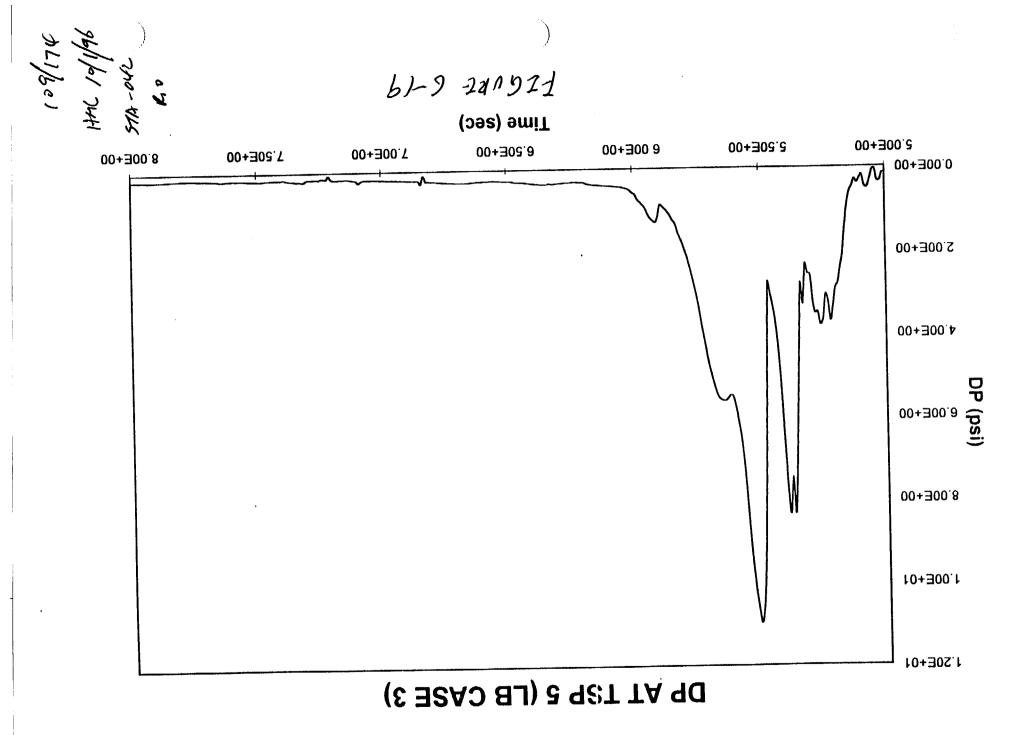




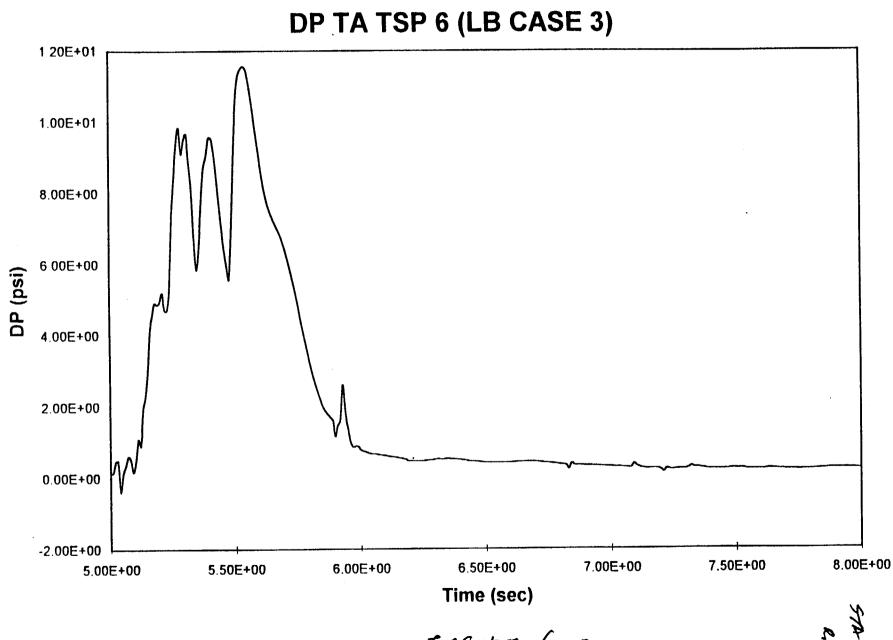
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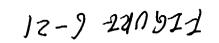


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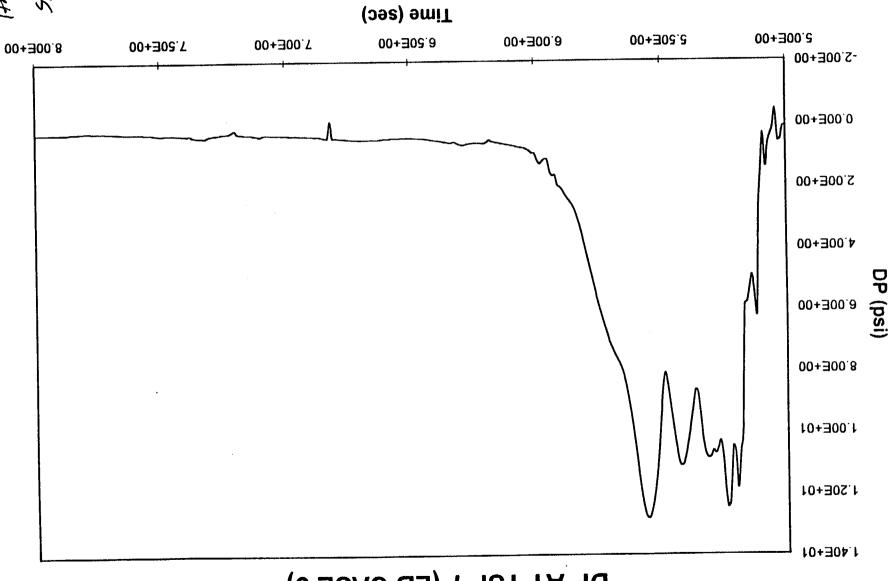
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FIGURE 6-20

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0.2 11/01 1041 11/01 1041



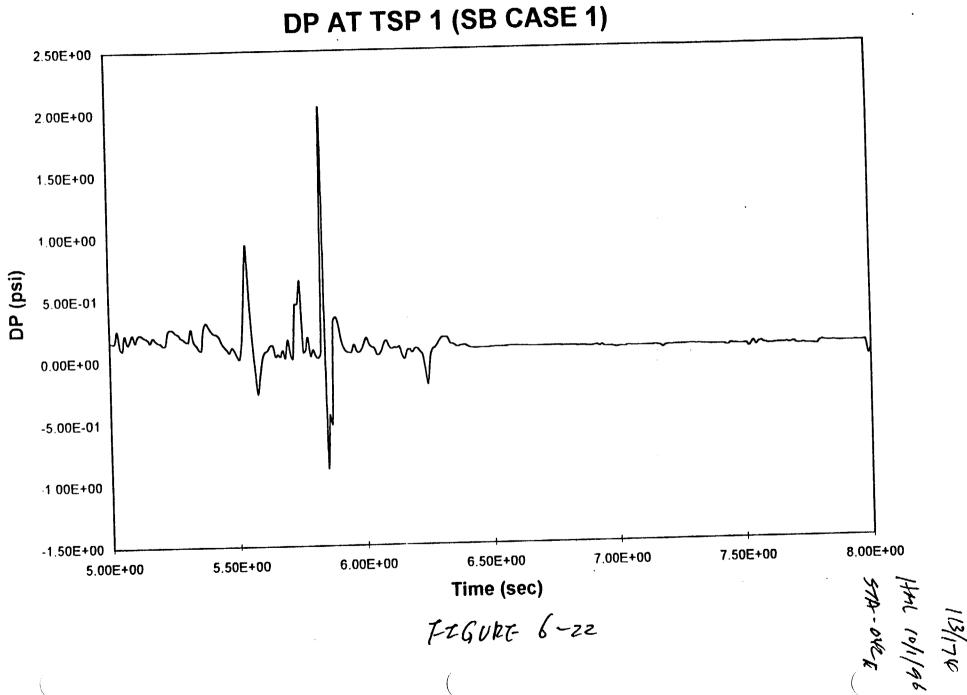
## DP AT TSP 7 (LB CASE 3)

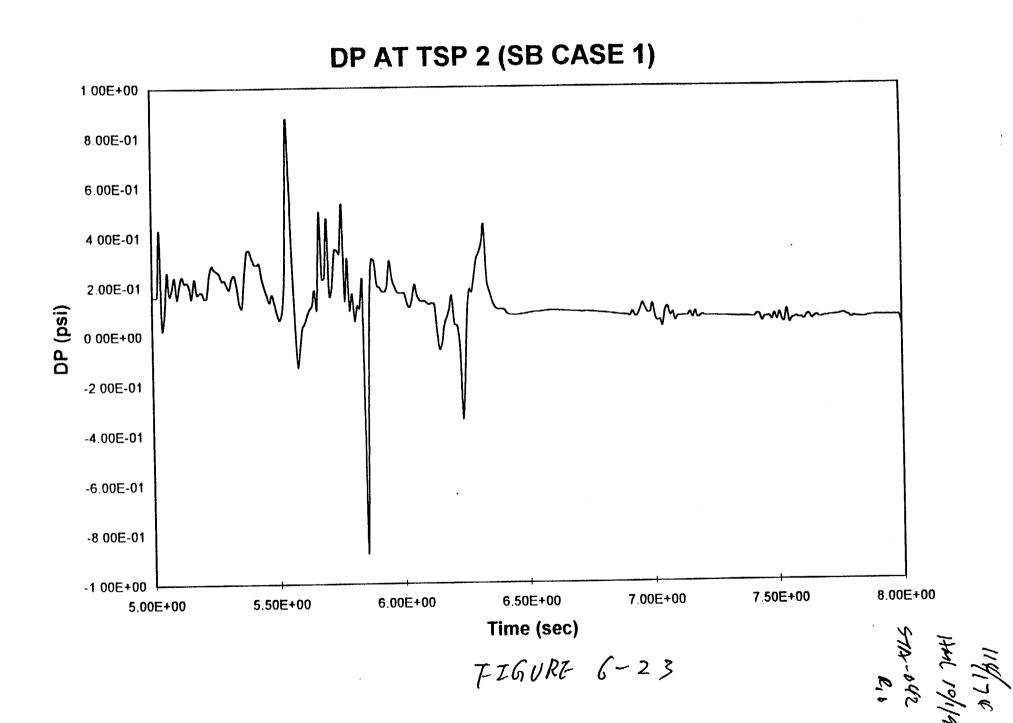
SHEET NO. 1/2 OF 174 SHEETS

1 and LB Case 3 indicates that the lower initial water level and higher TSP flow resistance used in LB Case 3 result in similar or lower differential pressures at the TSPs 1 to 3 (excluding the spikes for LB Case 3). However, for the TSPs at higher elevations (TSPs 4 to 7), the lower initial water level and higher TSP flow resistance used in LB Case 3 result in higher differential pressure and a higher differential pressure increase is calculated for a TSP at higher elevation.

#### Small Break Case 1

The time history of the differential pressures across TSPs 1 to 7 after the initiation of the break are plotted on Figures 6-22 to 6-28. The peak differential pressures across the TSPs 1 to 7 are 2.032 psi, 0.866 psi, 0.982 psi, 8.390 psi, 3.336 psi, 4.059 and 3.031 psi, respectively. As shown in Figure 6-22, 6-25 and 6-27, the peak differential pressure across TSPs 1, 4 and 6 for LB Case 3 are spikes with very short duration which can not be explained physically. Excluding the spikes, the peak differential pressures across the TSPs 1, 4 and 6 are 0.939 psi, 1.29 and 3.4 psi (approximate), respectively. All the peak pressures are occurred at 0.5 to 1.3 seconds after the initiation of the break. Similar to the large break cases, the duration of the high differential pressure across the TSP is very short for the TSP 1 which is located nearest to the bottom of the steam generator. The duration increases when the location of the TSP is further away from the bottom of the steam





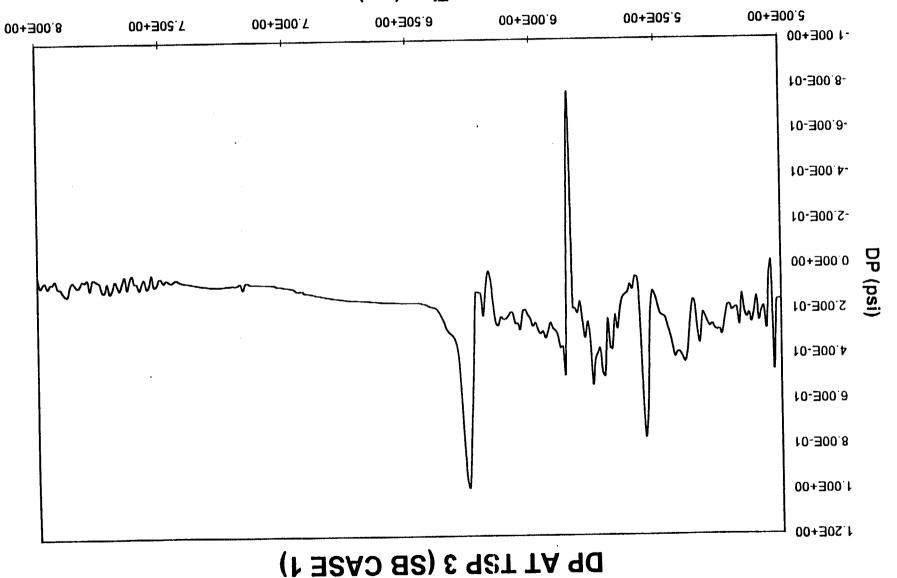
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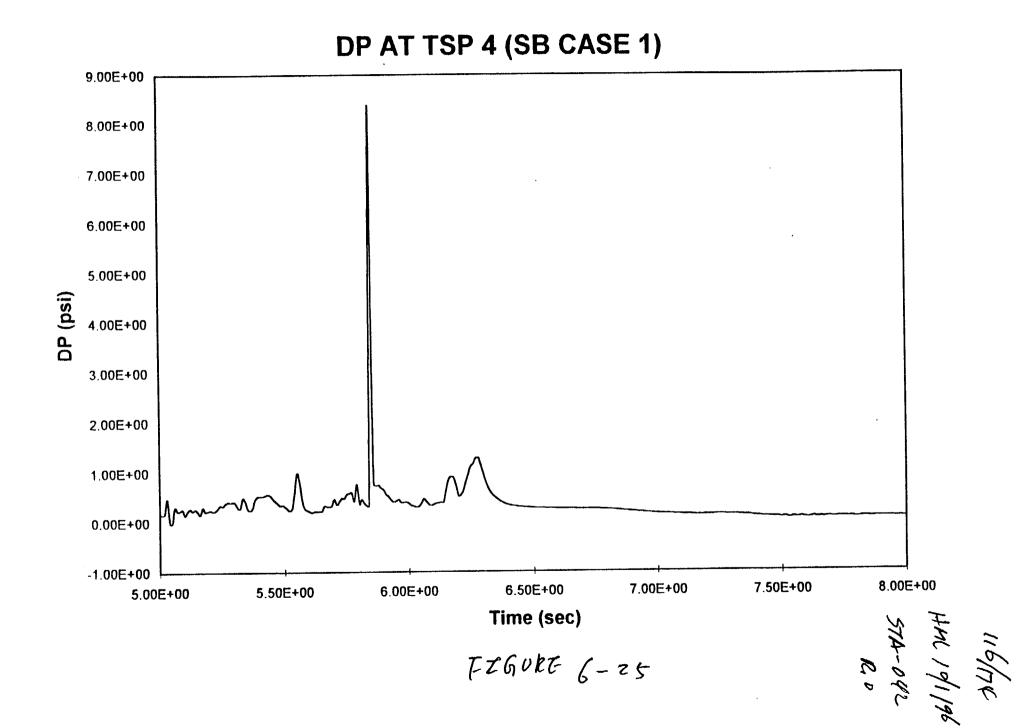
574 -04 R.o

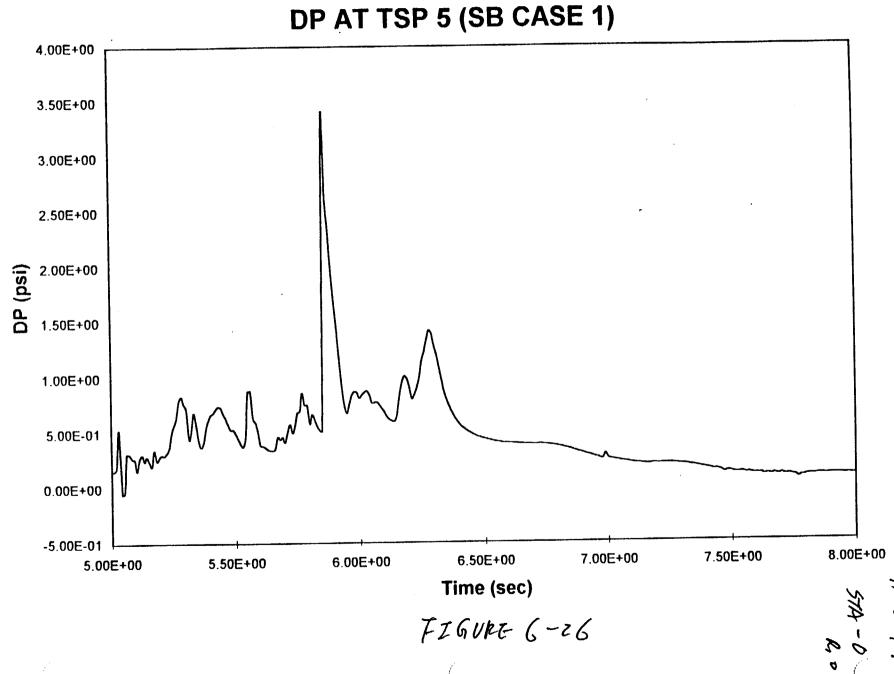
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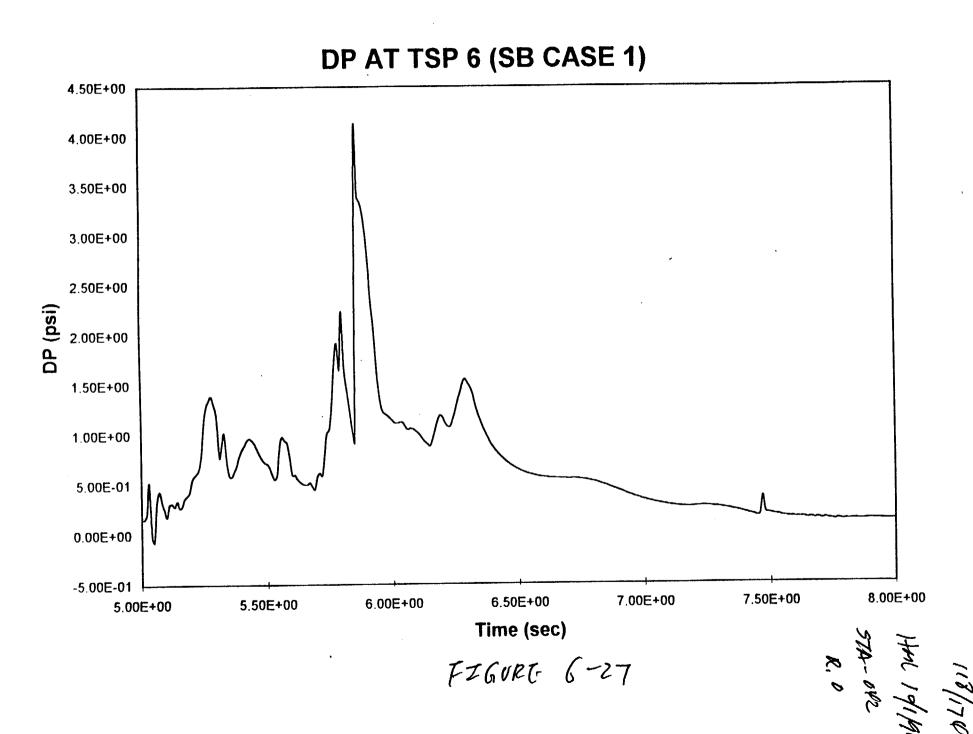






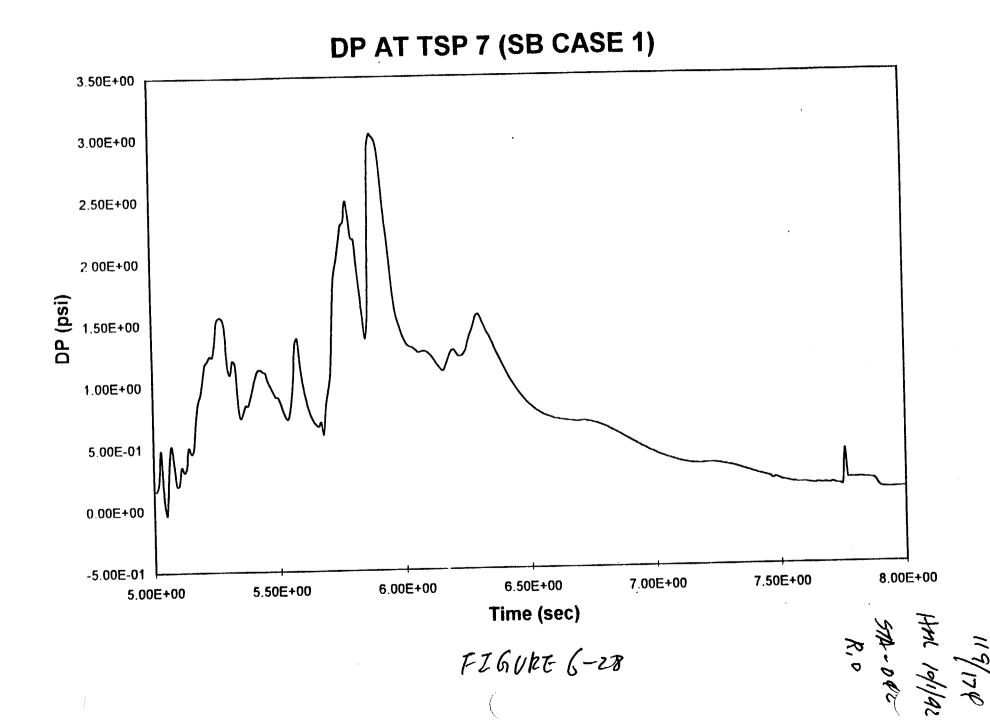
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SHEET NO. 120 OF 174 SHEETS CALC NO. STA-042 R. 0

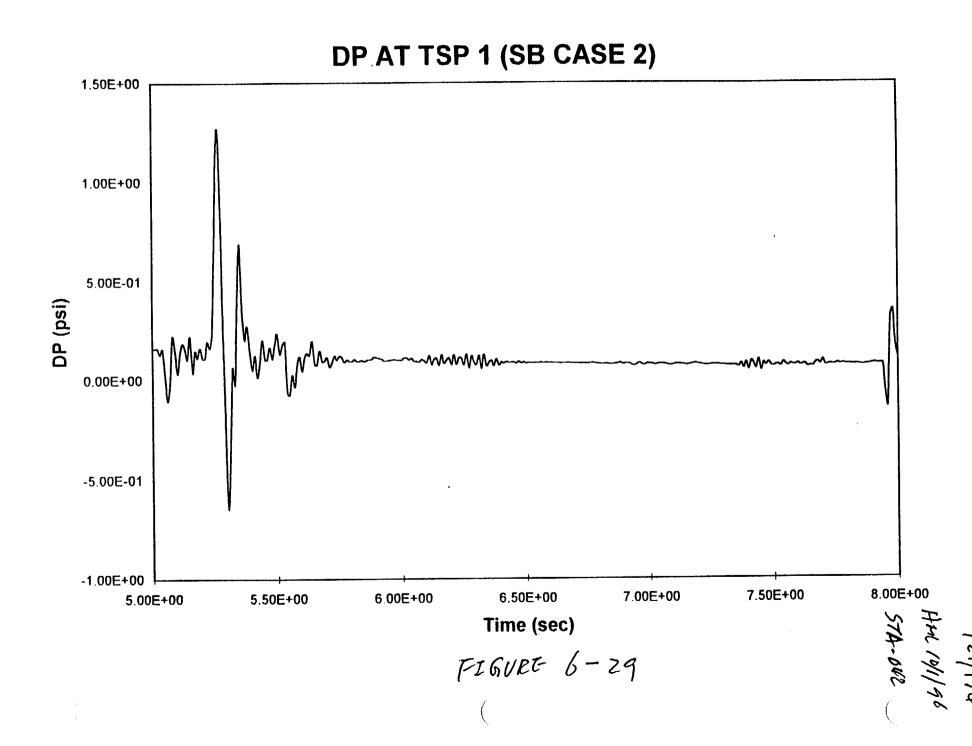
120/174

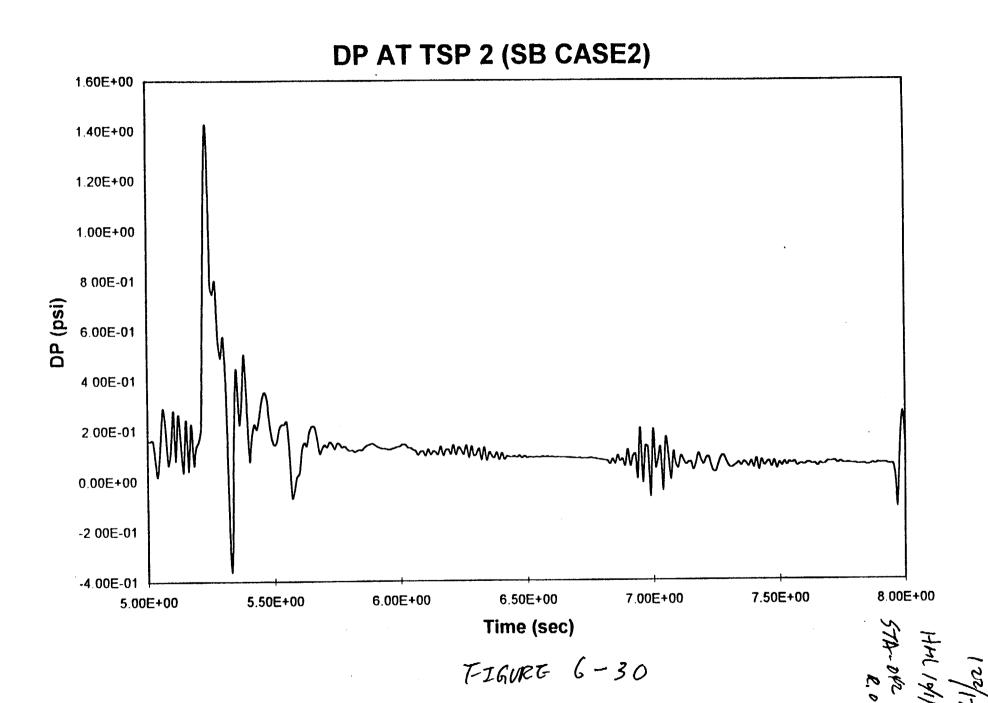
generator. Therefore, even the difference is very small between the peak differential pressures across the TSPs 3 to 7, the integrated force acting on the TSP increases with the elevation of the TSP.

#### Small Break Case 2

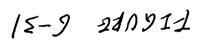
The time history of the differential pressures across TSPs 1 to 7 after the initiation of the break are plotted on Figures 6-29 to 6-354. The peak differential pressures across the TSPs 1 to 7 are 1.264 psi, 1.414 psi, 1.386 psi, 1.500 psi, 1.697 psi, 2.278 and 2.405 psi, respectively. Similar to the LB Case 2, the peak pressure across the TSP increases with the increase of the TSP elevation for LB Case 2 which is different from the SB Case 1. All the peak pressures are occurred within 0.5 second after the initiation of the break which is also much earlier than those for SB Case 1. In addition, more smooth time histories are noticed for the differential pressures acting on the TSPs for SB Case 2. Similar to SB Case 1, the duration of the high differential pressure across the TSP is very short for the TSP 1 which is located nearest to the bottom of the steam generator. The duration increases when the location of the TSP is further away from the bottom of the steam generator.

As discussed above, the characteristic of the differential pressures across the TSPs for SB Case 2 is substantially different from that for SB Case 1 which is a result of changing the modeling scheme from non-





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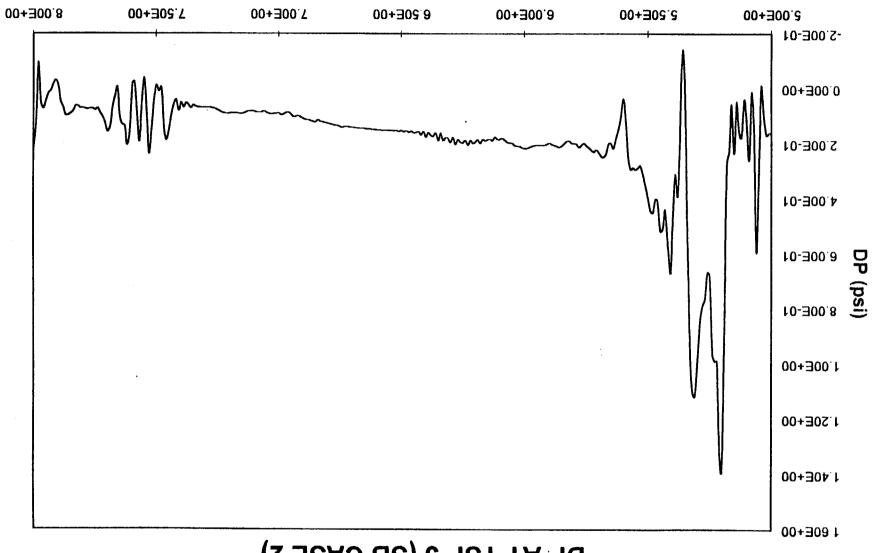
50

R

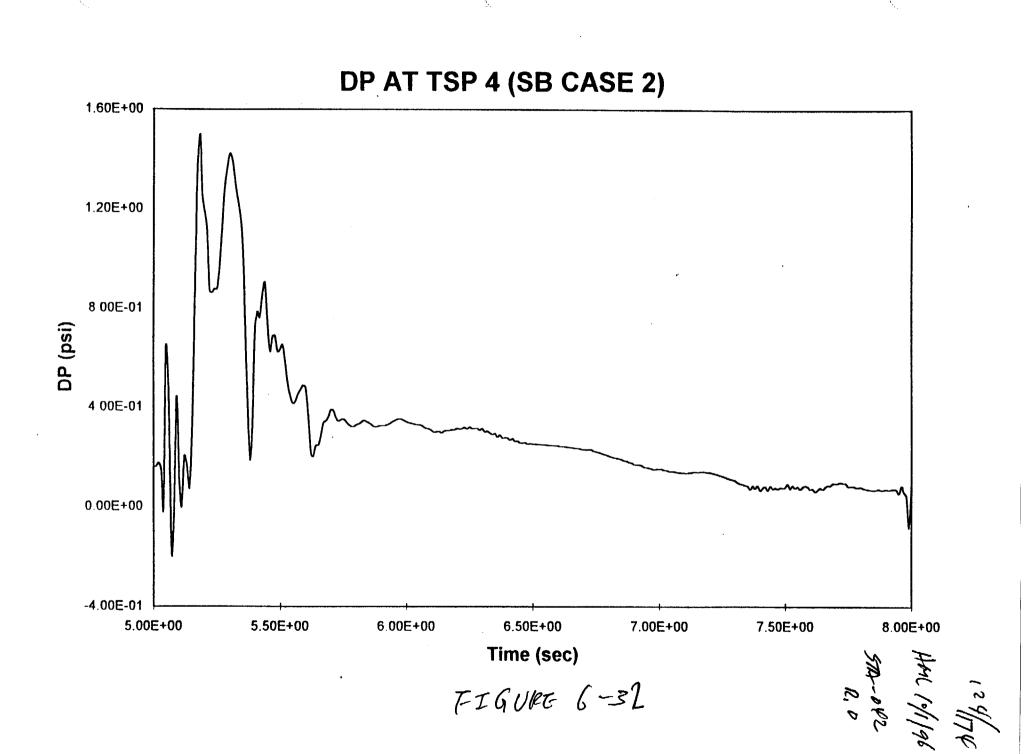
HMC 191

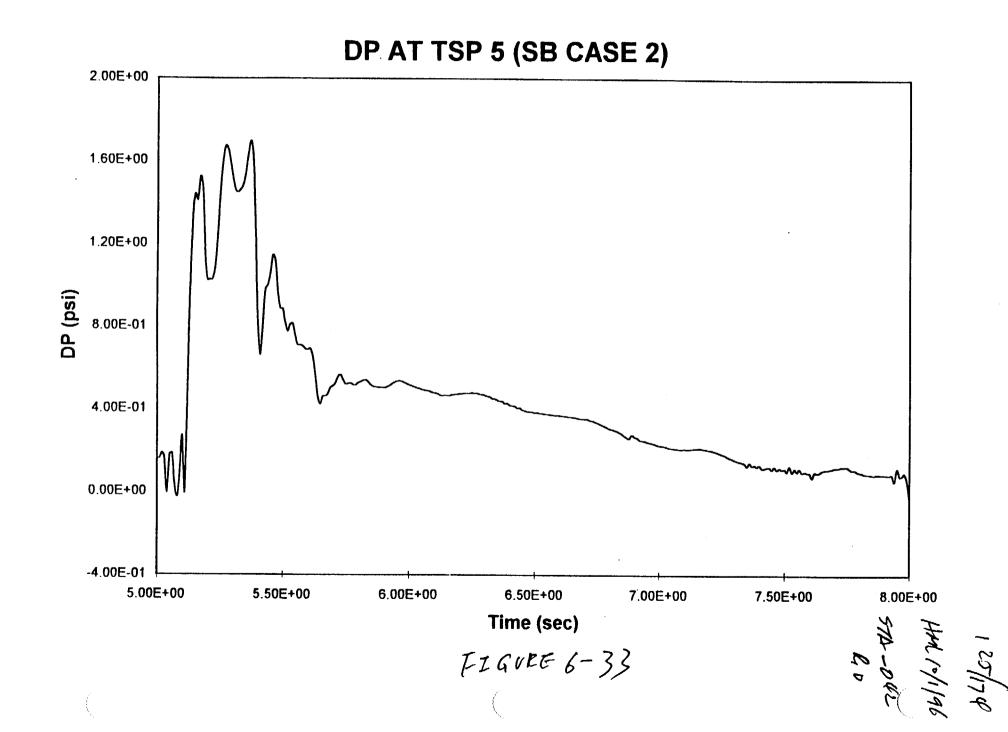
53

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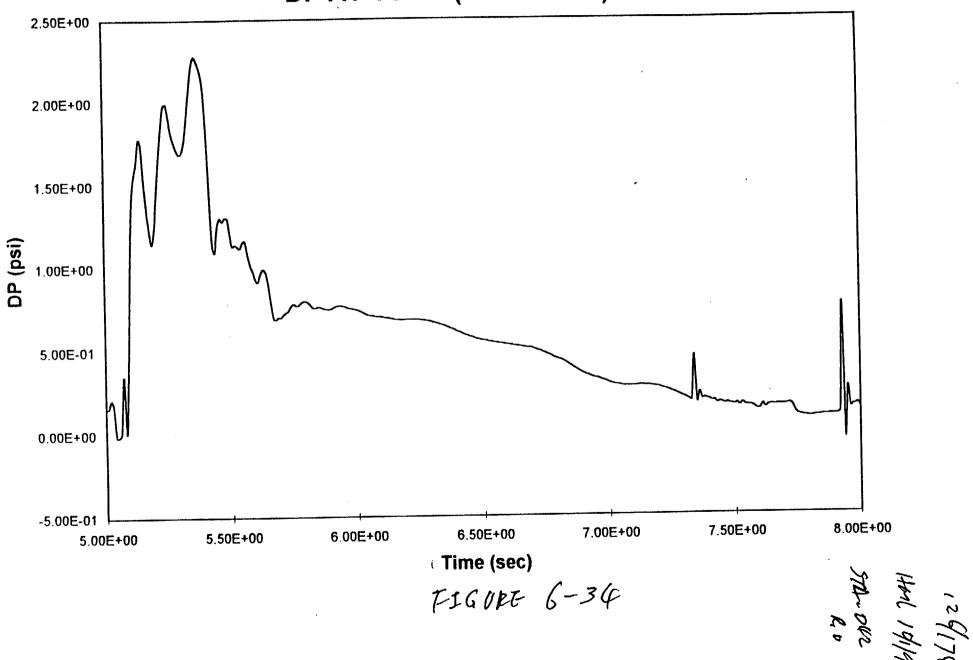
# DP AT TSP 3 (SB CASE 2)







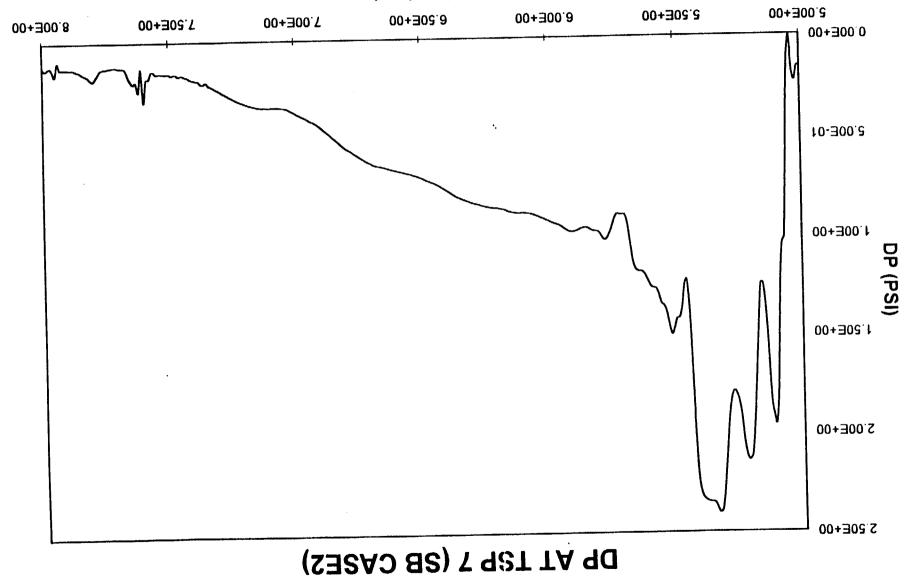
DP AT TSP 6 (SB CASE 2)



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1 2 7/14 1+11 19/121 590-022 6.

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SHEET NO.128 OF/74 SHEFTS CALC NO. STA-042 K, V Loads on the Steam Generator Support Plats During SLB Accident

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SUBJECT MADE BY H M Lee DATE 10/1/96 CHECK BY L R Chang APPROVED BY

equilibrium to equilibrium for the shell side of the tube region. It is difficult to determine which case is more accurate. Therefore, the results of both cases are transmitted to Westinghouse to perform structure analysis for the TSPs. However, since the extremely high differential pressures spikes calculated for some of the TSPs in SB Case 1 can not be explained physically, it may not be needed to consider these high spikes in the structure analysis.

#### DATA EXTRACTION FOR STP STRUCTURE ANALYSIS

The results of the RELAP5 analysis are transmitted to Westinghouse to perform structure analysis for the TSPs. In addition to the differential pressures across the TSPs, Westinghouse needs the pressure and density at the each TSP for their structure analysis . Therefore, the pressure and density at Volumes immediately above the TSPs are extracted from the RELAP5 output file with the differential pressures across the TSPs. The following input is used to extracting the data out from the RELAP5 output for each TSP.

#### TSP 1

The following STRIP run input is used to extract the time histories of the pressure, density and differential pressure which will be used in the structure analysis for the TSP 1.

=SLB pressure difference across the SG tube support plates 0000100 strip fmtout

#### SHEET NO.129 OF 174 SHEETS CALC NO. STA-042 R. P

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 103
 0

 1001
 p
 002040000

 1002
 rho
 002040000

 1003
 cntrlvar
 1

#### TSP 2

The following STRIP run input is used to extract the time histories of the pressure, density and differential pressure which will be used in the structure analysis for the TSP 2.

=SLB pressure difference across the SG tube support plates

0000100 strip fmtout

103 0

1001 p 002080000

1002 rho 002080000

1003 cntrlvar 2

•

#### <u>TSP 3</u>

The following STRIP run input is used to extract the time histories of the pressure, density and differential pressure which will be used in the structure analysis for the TSP 3.

=SLB pressure difference across the SG tube support plates 0000100 strip fmtout

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SUBJECT	Loads on the	Steam Generator	Support Plats	During SLB Accident
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103	0	
1001	р	002120000
1002	rho	002120000
1003	cntrl	var 3

#### TSP 4

The following STRIP run input is used to extract the time histories of the pressure, density and differential pressure which will be used in the structure analysis for the TSP 4.

=SLB pressure difference across the SG tube support plates

0000100 strip fmtout

103 0

1001 p 002160000

1002 rho 002160000

1003 cntrlvar 4

#### TSP 5

The following STRIP run input is used to extract the time histories of the pressure, density and differential pressure which will be used in the structure analysis for the TSP 5.

=SLB pressure difference across the SG tube support plates 0000100 strip fmtout

## SHEET NO. 13 OF 74 SHEETS CALC NO. STA-042 R. D

SUBJECT	Loads on the	Steam Generator	Support Plats	During SLB Accident
MADE BY_	H M Lee DATE	<u>10/1/96</u> CHECK	BY L R Chang	APPROVED

 103
 0

 1001
 p
 002200000

 1002
 rho
 002200000

 1003
 cntrlvar
 5

#### TSP 6

•

The following STRIP run input is used to extract the time histories of the pressure, density and differential pressure which will be used in the structure analysis for the TSP 6.

=SLB pressure difference across the SG tube support plates

0000100	strip	fmtout
103	0	
1001	р	002240000

1002 rho 002240000

1003 cntrlvar 6

#### <u>TSP 7</u>

The following STRIP run input is used to extract the time histories of the pressure, density and differential pressure which will be used in the structure analysis for the TSP 7.

=SLB pressure difference across the SG tube support plates 0000100 strip fmtout

			CI	ALC NO	STA-042 RO
SUBJECT	Loads on the	Steam Generator	Support Plats	During S	SLB Accident
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SHEET NO. 132 OF 174 SHEETS

 103
 0

 1001
 p
 002280000

 1002
 rho
 002280000

 1003
 cntrlvar
 7

Since the pressure and density data extracted from the RELAP5 output file are in the unit of pa and kg/m<sup>3</sup>. Microsoft Excel program is used to convert pa to psi by multiplying a factor of 1.45038e<sup>-4</sup> to the pressure data and convert kg/m<sup>3</sup> to lb/ft<sup>3</sup> by dividing a factor of 16.0185 to the density data. The names for the Excel files transmitted to Westinghouse are SLBLBC1.XLS, SLBLBC2.XLS and SLBLBC3.XLS for LB Cases 1, 2 and 3 and SLBSBC1.XLS and SLBSBC2.XLS for SB Cases 1 and 2. All these files are stored in two flappy disks which is attached as Attachment 1.

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SUBJECT <u>Loads on the Steam Generator Support Plats During SLB Accident</u> MADE BY <u>H M Lee</u> DATE <u>10/1/96</u> CHECK BY <u>L R Chang</u> APPROVED BY\_\_\_\_\_

- 7. References
  - Westinghouse Calculation TH-95-001, 'Model 51 Steam Generator TRANFLO Model Development', Dated 9/30/96.
  - Westinghouse Letter NCE-85-529, from NCD engineering to M.
     Oshinsky, " GENF Input for Models 44, 44F, 51, 51F and F Steam Generators", September 5, 1985. This letter is also attached to this calculation file as Appendix E.
  - 3. ASME Steam Table.
  - 4. RELAP5/Mod3 Code User's Manual.
  - WCAP-11206, Loss of Feed Flow, Steam Generator Tube Rupture and Steam Line Break Thermohydraulic Experiments.
  - 6. Nuclear Heat Transport, Published by ANS.
  - 7. Westinghouse Drawing 350794-B, "Steam Generator Nozzle to Elliptical Head". This Drawing is also attached to this calculation file as Appendix F.

# PACIFIC GAS AND ELECTRIC COMPANY<br/>GENERAL COMPUTATION SHEETSHEET NO.134 OF74 SHEETS<br/>CALC NO.SUBJECTLoads on the Steam Generator Support Plats During SLB AccidentMADE BYH M LeeDATE10/1/96CHECK BYL R ChangAPPROVED BY

Appendix A

Loss Coefficient of Tube Bundle Crossflow



F. 2/3 135/174 HM 10/1/96 STA-042 R.

NSD-JLH-6070

From:Steam Generator Design & AnalysisWIN:224-5992Date:March 7, 1996Subject:Loss Coefficient of Tube Bundle Crossflow for RELAP Modeling

To: M. J. Miller

NAME OF STREETS STRATE

cc: T. A. Pitterle G. P. Lilly W. J. Scherder

This is to respond to an action item generated during the March 6, 1996, reviewing meeting between Hsiung Lee and Westinghouse concerning the computer modeling of TRANFLO and RELAP for Model 51 steam generators. Please forward this to Hsiung Lee for his information and use.

The TRANFLO model for steam line break event considers a crossflow resistance across the tubesheet. The RELAP code may not have a built-in correlation for this crossflow resistance. It was agreed that Westinghouse should provide an equivalent corssflow loss coefficient for the use in the RELAP simulation.

The built-in correlation for the crossflow resistance in the TRANFLO code is as follows:

$$K = 192 \operatorname{Re}^{-0.145} \left(\frac{P}{De}\right)^{0.6} NL$$

where

 $Re_r = Reynolds$  number P = tube pitch De = hydraulic diameter $N_L = number of tube rows in crossflow$ 

The Reynolds number is defined as below:

$$\operatorname{Re}_{v} = \frac{\rho V_{\max} D e}{\mu}$$

MAR 7 '96 12:43

where

 $\rho =$ fluid density  $V_{max} =$  velocity through the tube gap  $\mu =$  dynamic viscosity

The hydraulic diameter is defined as below:

$$De = 4(\pi/4) [D_{iv}^2 - 2N_{vT} D_e^2] / [\pi (D_{iv} + 2N_{vT} D_e)]$$

where

 $D_{iw} = \text{inside diameter of wrapper}$  $N_{UT} = \text{number of U-tubes}$  $D_o = \text{outside diameter of U-tube}$ 

Now, for Model 51 steam generators,  $Diw = 123.50^{\circ}$ , NUT = 3388,  $Do = 0.875^{\circ}$ ,  $P = 1.2812^{\circ}$ . The TRANFLO model considers NL = 24 for effective crossflow at the tubesheet. Therefore, it follows that  $De = 1.6628^{\circ}$ . Finally, we obtain the following

 $K = 39.4 \,\mathrm{Re}^{-\omega \omega}$ 

At a Reynolds number of  $1.0 \ge 10^6$ , K = 5.32, and at a Reynolds number of  $2.0 \ge 10^6$ , K = 4.81. Note that  $V_{max}$  for Reynolds number is based on a flow area of 4.43 ft<sup>2</sup> for the crossflow. Consider that  $V_{max} = 10$  ft/sec of saturated water at 1000 psia, it follows that Re =  $46.32 \ge 10 \ge 1.6628/(12 \ge 0.00006293) = 1.02 \ge 10^6$ .

Considering the above discussion, we recommend, as an approximation, to use K = 5.32 in the RELAP calculation.

M. H. Hu SG Design and Analysis

Approved:

J. L. Houtman, Manager SG Design and Analysis

P.3/3

136/174 1411 10/1196 STA-042 RO

## PACIFIC GAS AND ELECTRIC COMPANY

 GENERAL COMPUTATION SHEET
 SHEET NO 137 OF 174 SHEETS CALC NO. STA-042 R v

 SUBJECT
 Loads on the Steam Generator Support Plats During SLB Accident

 MADE BY
 H M Lee
 DATE 10/1/96 CHECK BY
 L R Chang APPROVED BY

Appendix B

Sensitivity Study for Initial Steam Generator Water Level

#### CALC NO. STA-042 K v SUBJECT Loads on the Steam Generator Support Plats During SLB Accident MADE BY H M Lee DATE 10/1/96 CHECK BY L R Chang APPROVED BY

SHEET NO. 138 OF 174 SHEETS

As discussed in Section 5, void fraction used in the TRANFLO model is input into RELAP5 model as quality. A sensitivity study is performed in this Appendix to show that the RELAP5 model is conservative. The LB Case 2 is reanalyzed in LB Case 4 with changing the void fractions used for Volumes 23-01, 32-01, 33-01, 53-01 and 36-01 to water qualities. The equation 12-3a of Reference 6 gives the relation between void fraction and water quality as follows.

F = (X \* Vg) / (Vf + X \* Vfg)

where F = void fraction

X = water quality

Vf = specific volume for water

Vg = specific volume for steam

Vfg = Vg - Vf

The above equation can be rewritten as:

F \* Vf + X \* F \* (Vg - Vf) = X \* VgX \* (Vg - F \* Vg + F \* Vf) = F \* Vf X = (F \* Vf)/((1-F) \* Vg + F \* Vf)

For Volume 23-01, the pressure is 1022.72 psia. The specific volumes for saturated water and steam at 1022.72 psia are 0.02167 ft<sup>3</sup>/lbm and 0.43491 ft<sup>3</sup>/lbm. Then, the water quality for void fraction 0.03 is 0.00154.

For Volume 32-01, the pressure is 1021.26 psia. The specific volumes for saturated water and steam at 1021.26 psia are 0.02167  $ft^3/lbm$  and 0.43560

#### CALC NO.\_\_\_\_STA-042<u>*K.G*</u> SUBJECT <u>Loads on the Steam Generator Support Plats During SLB Accident</u> MADE BY H M Lee DATE 10/1/96 CHECK BY<u>L R Chang</u> APPROVED BY\_\_\_\_\_\_

SHEET NO. 13 TOFJ74

ft<sup>3</sup>/lbm. Then, the water quality for void fraction 0.92 is 0.364.

For Volumes 33-01 and 53-01, the pressure is 1021.72 psia. The specific volumes for saturated water and steam at 1021.72 psia are 0.02167 ft<sup>3</sup>/lbm and 0.43539 ft<sup>3</sup>/lbm. Then, the water quality for void fraction 0.73 is 0.119.

For Volume 36-01, the pressure is 1021.57 psia. The specific volumes for saturated water and steam at 1021.57 psia are 0.02167 ft<sup>3</sup>/lbm and 0.43546 ft<sup>3</sup>/lbm. Then, the water quality for void fraction 0.83 is 0.195.

The following input change are used in the reanalysis.

0230200 1022.72 0.00154 2 0320200 2 1021.26 0.364 1021.72 0.119 0330200 2 0530200 2 1021.72 0.119 1021.57 0.195 0360200 2

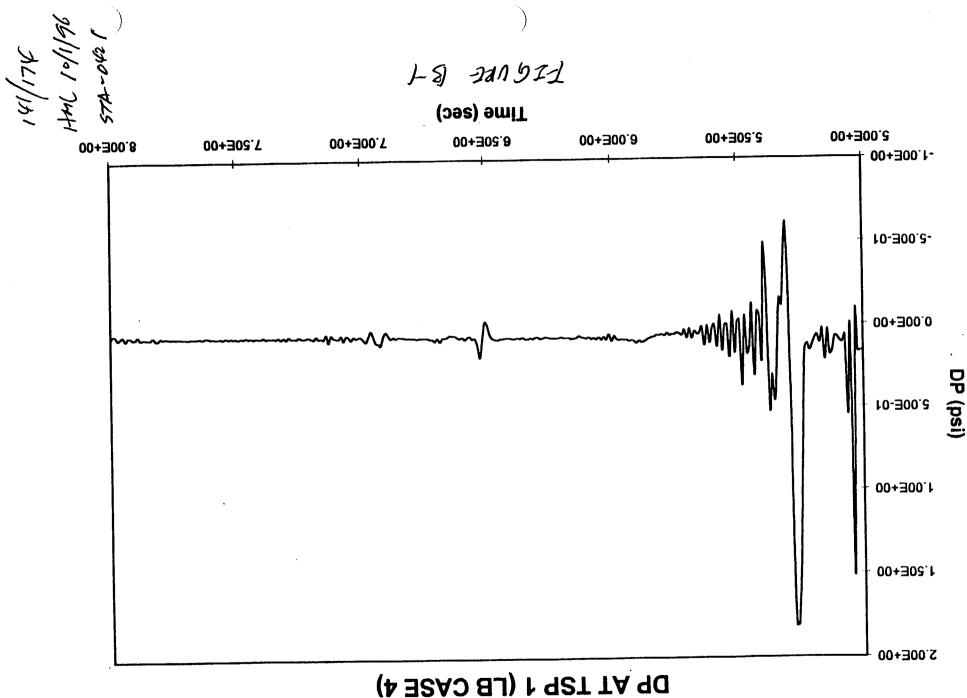
The remain input is the same as those used for LB Case 2. The input file name is reidp6 and the output file name is reodp6.

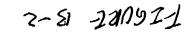
The results of the LB Case 4 are microfiched and attached in the Appendix G. The time history of the differential pressures across TSPs 1 to 7 after the initiation of the break are plotted on Figures B-1 to B-7. The peak differential pressures across the TSPs 1 to 7 are 1.814 psi, 2.116 psi, 2.559

SUBJECT

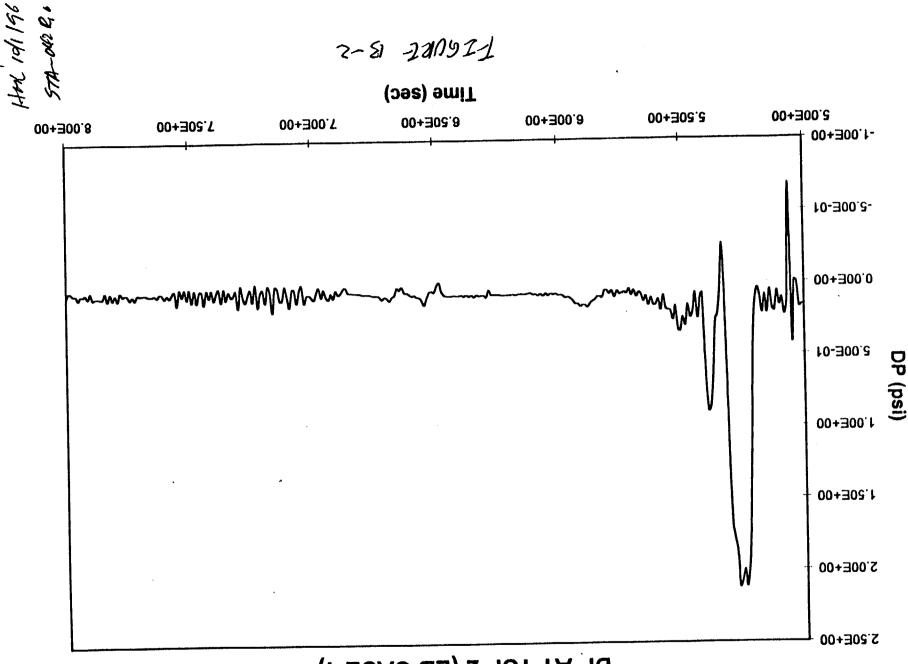
SHEET NO. 140 OF (74 SHEETS CALC NO. STA-042 R0 Loads on the Steam Generator Support Plats During SLB Accident MADE BY H M Lee DATE 10/1/96 CHECK BY L R Chang APPROVED BY

psi, 3.987 psi, 5.733 psi, 7.814 and 9.130 psi, respectively. The time history curves for the differential pressure across the TSPs for LB Case 4 are very similar to those for LB Case 2. The magnitude of the differential pressure across the TSPs for LB Case 4 are smaller then those for LB Case 2. Therefore, it can be conclude that the RELAP5 model used in this calculation is conservative.



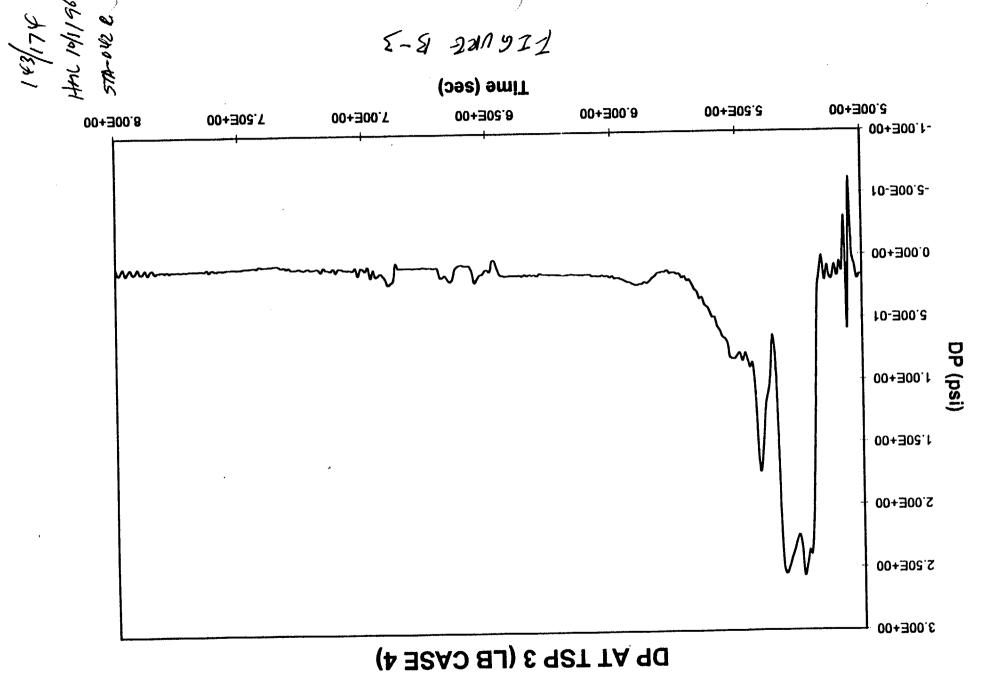


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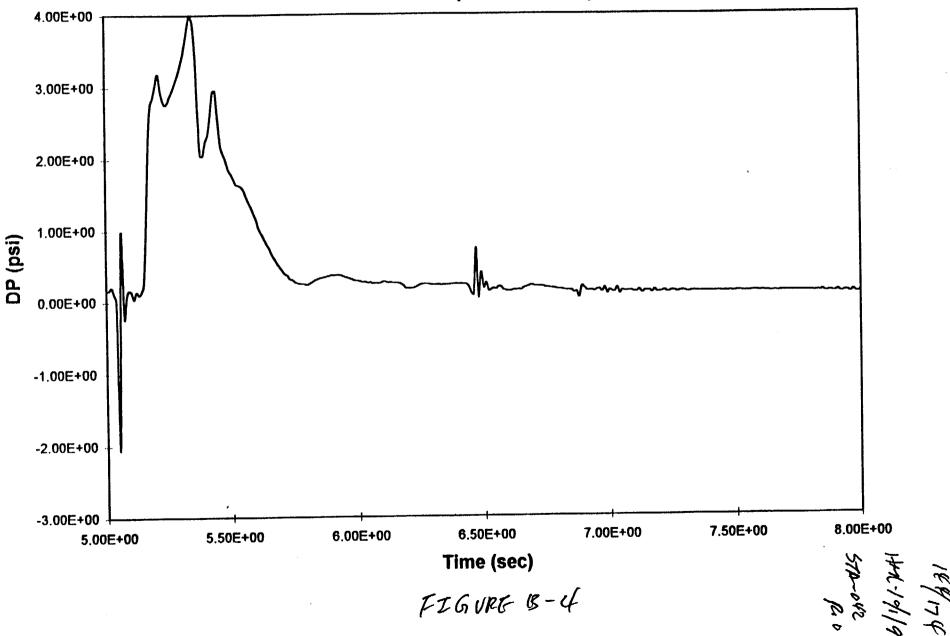


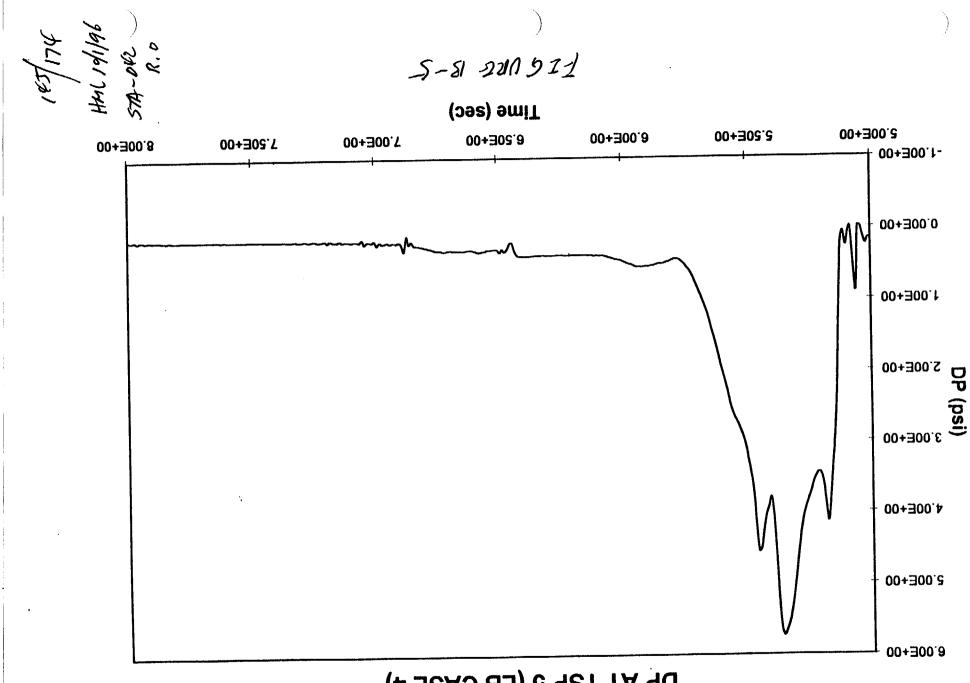
## DP AT TSP 2 (LB CASE 4)

5-8 221911

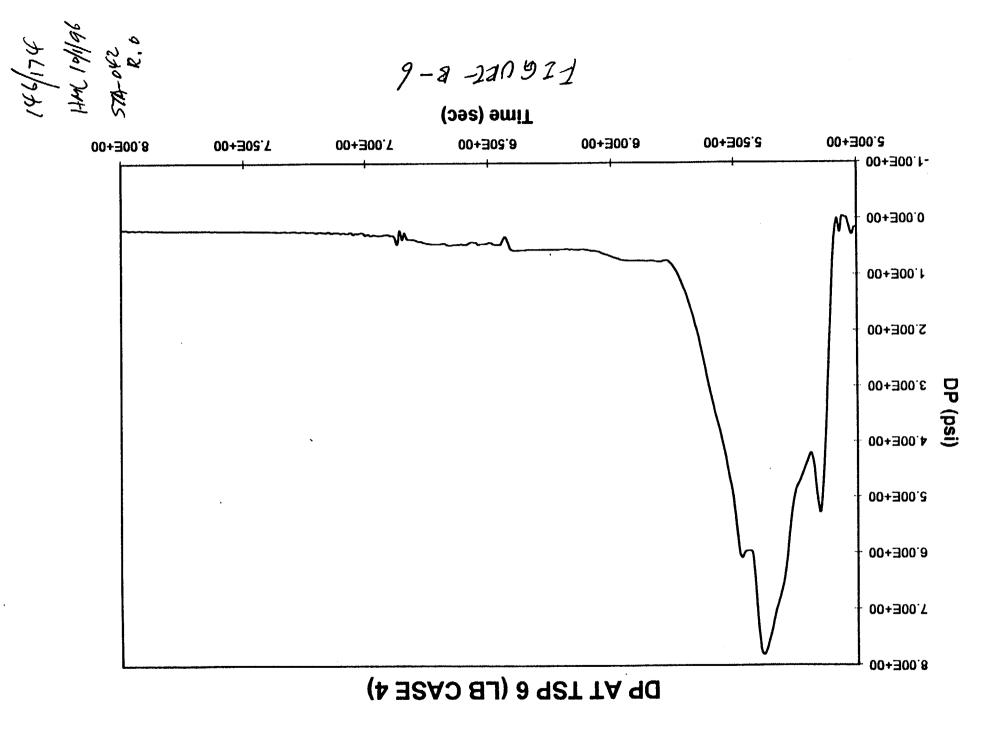


DP AT TSP 4 (LB CASE 4)



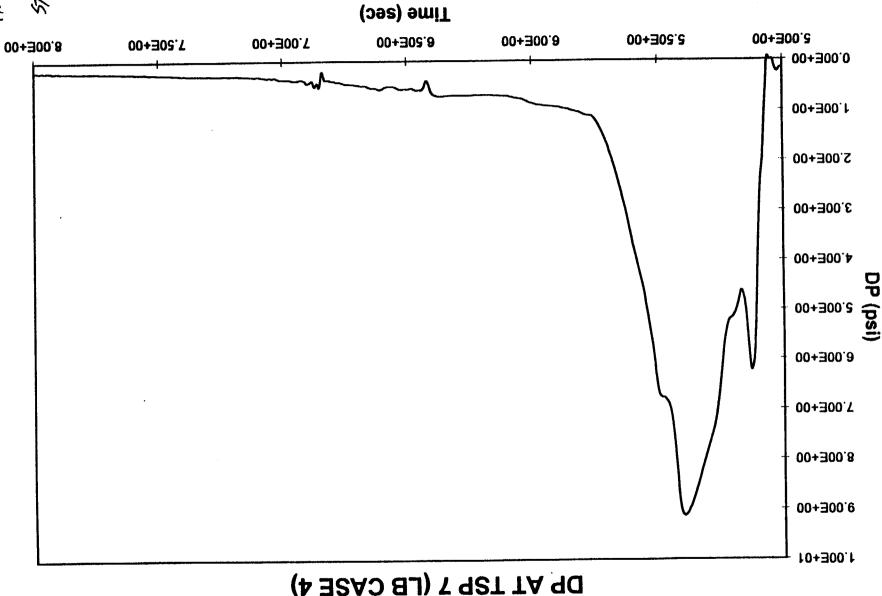


## DP AT TSP 5 (LB CASE 4)



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PACIFIC GAS AND ELECTRIC COMPANY	SHEET NO. 1905/79 SHEETS
GENERAL COMPUTATION SHEET	CALC NO. STA-042 R.O.
	CALC NO. STA-042 R.O tor Support Plats During SLB Accident CK BY L R Chang APPROVED BY

Appendix C

Tranflo Input Changes for Case 61

#### MAR 08 796 02:19PM SGT&E

Nodes for Water level Nodes for Water HANL 10/1/96 STA-042 R. D stors 3. 131 De Porent sicy-1 and mor SID -Mominal Level (490°) - DER 0.03 1022.72 \$47 38.57 244.3 28 0 0.92 1021.26 547 42.97 \$6.73 8 0.73 1021.72 547 42.04 688.6 13 ۵ 3} Connectors 3. \$ 31, D.e. Resist. 1021.57 \$47 Connectors 34-40 TSP loss weft 43.52 22.83 36 0.5 .4275 0.5 17.74 1.548 0.5 0.5 17.74 .4275 1.548 0.78 :3.716 0.0625 0.0625 0.78 0.78 :3.716 0.0625 0.0625 0.78 0.78 13.716 0.8625 0.0625 0.78 0.74 13.716 0.0625 0.0625 0.78 Casel Cards lo 3 1.716 0.0625 0.0625 0.78 0.78 13.716 0.0625 0.0625 0.78 0.78 3 be Schanged for ... Case 61 0.74 13.716 0.0625 0.0625 0.78

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FROM OPL LICENSING

1212V-1	TOB ALZ	STD -No	EST CASO	(CASO 6)	5		
13	0	244.3	38.57	1022.17		0.39	0
32	D	\$6.73	42.97	1021.28	547	1	C
33	8	688.6	42.04	1021.28	\$47	0.93	0
36	D	22.83	43.52	1021.07	547	1	• • •
3. <b>54</b> 8	17.74	.4275	0.0	0.0	3		
3.548	17.74	.4275	0.0	0.0	3		
23.716	0.0625	0.0625	0.93	0.99	3		
13.716	0.0625	0.0625	0.99	0.99	3		
21.716	0.0625	0.0625	0.99	0.99	3		
23.716	0.0625	0.0625	0.99	0.99	3		
23.716	0.0625	0.0625	0.99	0.99	3		
23.715	0.0625	0.0623	9.99	0.99	3		
23.716	0.0625	0.0625	0.99	0.99	3		

Case 61 carols changed from Case 1

## PACIFIC GAS AND ELECTRIC COMPANY GENERAL COMPUTATION SHEET SHEET NO(5° OF /74 SHEETS CALC NO. SUBJECT Loads on the Steam Generator Support Plats During SLB Accident MADE BY H M Lee DATE 10/1/96 CHECK BY L R Chang APPROVED BY

Appendix D

Input Listing for LB Case 1

=SLB pressure difference across the SG tube support plats \* hot standby nonequilibrium models \* 100 new transnt \* british british 102 105 \* \*\*\*\*\*\* time step cards \* \* \* 10000 200 3 2 0.005 1.d-7 201 5. 100000 20000 0.00001 1000 3 1.d-7 5.3 202 100000 400 8000 3 1.d-7 0.000025 6.5 203 10000 100000 200 3 0.00005 1.d-7 8.0 204 100000 10000 3 100 0.00010 1.d-7 205 1000.0 \* \* \* \* minor edit variables \* \* \* 518000000 mflowj 301 002030000 mflowj 302 002070000 303 mflowj 002110000 mflowj 304 002150000 305 mflowj 002190000 3 mflowj 002230000 mflowj 3... 002270000 308 mflowj 017010000 309 р 018010000 \*310 р 019010000 \*311 р 020010000 \*312 р 021010000 \*313 р 022010000 \*314 p 023010000 \*315 p 033010000 \*316 p 034010000 \*317 p 036010000 \*318 p 1 319 cntrlvar 2 cntrlvar 320 3 cntrlvar 321 4 cntrlvar 322 5 323 cntrlvar 6 cntrlvar 324 7 cntrlvar 325 \* \* \* \* \*\*\*\*\* \*\*\*\* trip input data + 8.0 1 null 0 0 ge

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1000200
                  2235.7
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1000202
                   800.0
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                    800.0
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                          547.0
           5.0
                 2200.0
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1010203
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                pipe
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0010001
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0010101
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0010301
          1.1667
                    3
          1.2553
0010302
                    5
          0.5
0010303
                    7
          1.60435
0010304
                    9
0010305
          0.5
          1.60435
                    11
0010306
          0.5
                    13
0010307
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0010308
          1.60435
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0010309
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0010310
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          0.5
0010311
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          1.60435
0010312
                    25
0010313
          0.5
          1.60435
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0010314
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          3.0
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0010316
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          1.60435
0010319
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0010320
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0010322
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45 )010323 0.5 1.60435 47 )010324 0.5 49 0010325 1.60435 51 ं **२**26 on: 53 0.5 JL 27ز 55 1.60435 0010328 57 0.5 )010329 59 1.2553 )010330 60 0010331 1.1667 30 90.0 0010601 60 0010602 -90.0 60 0.0642 0.0 0010801 00000 60 0011001 59 000000 0011101 0.0 0.0 0.0 547.0 3 2250.0 0011201 0011300 1 59 0.0 0.0 9148.5 0011301 \* tmdpjun prminl 5000000 10.956 1000000 100000000 5000101 1 5000200 0.0 0.0 9148.5 0.0 5000201 0.0 9148.5 0.0 1.0e6 5000202 \* \* tmdpjun 5010000 prmout 10.956 101000000 5010101 1010000 1 5010200 9148.5 0.0 0.0 0.0 Ξ .201 0.0 0.0 9148.5 1.0e6 5L\_J202 \* ÷ 0020000 shell pipe 30 0020001 27 54.22 0020101 30 70.0 0020102 54.22 2 0020201 3 23.716 0020202 6 54.22 0020203 7 23.716 0020204 10 54.22 0020205 23.716 11 0020206 14 54.22 0020207 15 23.716 0020208 18 0020209 54.22 23.716 19 0020210 22 54.22 0020211 23 23.716 0020212 26 54.22 0020213 27 0020214 23.716 70.0 29 0020215 1 1.2553 0020301 2 1.2553 0020302 4 n==0303 0.5 6 J304 1.60435 0.5 8 0020305 1.60435 10 0020306 12 0020307 0.5 1.60435 14

0020308

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15\$174 1+ML 10/196 57A-042,

0020309         0020310         0020311         00112         01113         01113         0120314         0120315         0120316         0020317         0020601	0.5 16 1.60435 18 0.5 20 1.60435 22 0.5 24 1.60435 26 0.5 28 3.2075 29 3.4338 30 90.0 30	-			
0020801 0020802	0.00015 0	.136 .0	29 30		
0020901 0020902	0.0 0.0 0.78 0.78	2 3			
0020903	0.0 0.0	6 7			
0020904 0020905	0.0 0.0	10			
0020906	0.78 0.78 0.0 0.0	11 14			
0020907 0020908	0.78 0.78	15			
0020909 0020910	0.0 0.0 0.78 0.78	18 3 19			
0020911	0.0 0.0	22			
0020912 0020913	0.78 0.78 0.0 0.0	3 23 26			
0020914	0.78 0.78	3 27			
0020915 0021001	0.0 0.0 00100 29	29			
0071002	00000 30	)			
0 101 0 201	000000 29 3 1033.73	9 547.0	0.0	0.0	0.0
0021202	3 1033.34	547.0	0.0	0.0	0.0 0.0
0021203 0021204	3 1033.07 3 1032.91	547.0 547.0	0.0 0.0	0.0 0.0	0.0
0021205	3 1032.57	547.0	0.0	0.0	0.0
0021206 0021207	3 1032.06 3 1031.72	547.0 547.0	0.0 0.0	0.0 0.0	0.0 0.0
0021208	3 1031.56	547.0	0.0	0.0	0.0 0.0
0021209 0021210	3 1031.22 3 1030.71	547.0 547.0	0.0 0.0	0.0 0.0	0.0
0021211	3 1030.37	547.0	0.0	0.0	0.0 0.0
0021212 0021213	3 1030.21 3 1029.87	547.0 547.0	0.0 0.0	0.0 0.0	0.0
0021214	3 1029.36	547.0	0.0	0.0	0.0 0.0
0021215 0021216	3 1029.02 3 1028.86	547.0 547.0	0.0 0.0	0.0 0.0	0.0
0021217	3 1028.53	547.0	0.0	0.0 0.0	0.0 0.0
0021218 0021219	3 1028.01 3 1027.68	547.0 547.0	0.0 0.0	0.0	0.0
0021220	3 1027.52	547.0	0.0	0.0 0.0	0.0 0.0
0021221 0021222	3 1027.18 3 1026.66	547.0 547.0	0.0 0.0	0.0	0.0
0021223	3 1026.33	547.0	0.0 0.0	0.0 0.0	0.0 0.0
0021224 C 1225	3 1026.17 3 1025.83	547.0 547.0	0.0	0.0	0.0
1226	3 1025.32	547.0	0.0 0.0	0.0 0.0	0.0 0.0
0021227 0021228	3 1024.98 3 1024.82	547.0 547.0	0.0	0.0	0.0
0021229	3 1024.23	547.0	0.0	0.0 0.0	0.0 0.0
0021230	3 1023.17	547.0	0.0	0.0	0.0

154/174 HML 10/1/96 STA-042 R.D

155/174 HML 10/1/96 0021300 1 29 0.0 0.0 0.0 0021301 1.0 29 1.0 0.0 0.0625 0021401 5TA-042 K 0350000 downc pipe 2350001 3 3 0.0 3350101 7.096 2 0350201 11.827 3 0350301 3 122.4 0350401 3 -90.0 0350601 0.4275 3 0.00015 0350801 00000 3 0351001 000000 2 0351101 1 0.0 0.0 0.0 3 1024.84 547.0 0351201 2 0.0 0.0 547.0 0.0 3 1028.64 0351202 0.0 3 547.0 0.0 0.0 3 1032.44 0351203 0351300 1 2 0.0 0.0 0.0 0351301 \* branch tubesh 0300000 2 1 0300001 0.136 00100 0.00015 90. 1.1667 1.1667 Ο. 54.22 0. 0300101 547.0 1034.15 3 0300200 000000 0.5 0.5 7.096 030000000 035010000 0301101 000000 5.32 5.32 4.43 002000000 030010000 0302101 0.0 0.0 0.0 0301201 0.0 0.0 0.0 201 \* feedrg branch 0340000 1 0340001 1 0.00015 0.0 00000 0. -90. -3.1097 3.1097 0.0 92.1 0340101 547.0 1022.48 0340200 3 0.0 000100 035000000 7.096 0.0 034010000 0341101 0.0 0.0 0341201 0.0 4 abovetb snglvol 0230000 00000 0.00015 0.0 4.9423 0.0 0.0 90. 4.9423 49.43 0230101 1022.72 0.03 2 0230200 4 abovetb sngljun 5330000 0.0 000100 49.43 0.0 002010000 023000000 5330101 1.0 1.0 0.0 0.0 5330110 0.0 0.0 0.0 1 5330201 \* \* speratr separatr 0220000 3 1 0220001 00000 0.0 0.00015 90. 3.9156 0. 3.9156 0.0 41.73 0220101 1021.14 1.0 0220200 2 000000 0.84 0.47 12.828 021000000 1101 022010000 0.597 0.597 000000 17.35 022000000 032000000 JZ22101 000000 8.689 8.689 41.73 022000000 023010000 0223101 0.0 0.0 0.0 0221201 0.0 0.0 0.0 0222201

155/17P HML 19/196 STD-042 0223201 0.0 0.0 0.0 ٠ 020000 liqsept snglvol 0.00015 0.0 00000 0.0 0. 0.0 0.0 86.75 .01 17.35 0. 0320200 2 1021.26 0.92 -\* 0330000 abovf1 branch 0330001 2 1 0.0 00000 0.0 0.0 -90.0 -2.9225 0.00015 100.7 2.9225 0330101 1021.72 0.73 2 0330200 033000000 0.0 17.35 0.0 000000 032010000 0331101 034000000 79.288 0.0 0.0 000000 0332101 033010000 0.0 0.0 0.0 0331201 0.0 0.0 0.0 0332201 ÷ \* abovfr2 branch 0530000 0530001 2 1 0.0 0.0 -90.0 -3.9156 00000 3.9156 0.00015 0.0 100.7 0530101 1021.72 0.73 2 0530200 0.5 0.5 000000 053000000 2.34 036010000 0531101 053010000 033000000 100.7 0.0 0.0 000000 0532101 0.0 0.0 0.0 0531201 0.0 0.0 0.0 0532201 \* \* 0210000 abovspr branch 201 2 1 0 0.0 90. 2.281 0.00015 0.0 00000 2.281 0.0 152.19 0. 101 1021.12 1.0 0210200 2 020000000 70.75 0.0 0.0 000100 021010000 0211101 7.96 1.78 1.67 000000 053000000 0212101 021000000 0.0 0.0 0.0 0211201 0.0 0.0 0.0 0212201 \* \* spsteam snglvol 0200000 90. 7.4502 0.00015 0.0 00000 7.4502 0.0 0.0 70.75 0200101 2 1020.96 1.0 0200200 \* \* dryer separatr 0190000 1 0190001 3 0. 0. 0.00015 0.0 00000 0.7083 0.0 0. 171.4 0190101 2 1020.96 1.0 0190200 5.502 5.502 000000 018000000 63.49 019010000 0191101 0.5 000000 019000000 036000000 2.34 0.5 0192101 0.5 0.5 000000 020010000 019000000 70.75 0193101 0.0 0.0 0.0 0191201 0.0 0192201 0.0 0.0 0.0 0.0 0.0 0193201 dsdryer snglvol 000 λĽ 0.00015 0.0 00000 2.34 0.0 -90. -9.7312 9.7312 0.0 0360101 2 1021.57 0360200 0.82 \*

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11201522	001420000	10000	1	0	1095.61 43
11201523	001440000	10000	1	0	341.45 45
11201524	001460000	10000	1	0	1095.61 47
11 1.525	001480000	10000	1	Ō	341.45 49
		10000	1	Õ	1095.61 51
11526	001500000				341.45 53
11201527	001520000	10000	1	0	
11201528	001540000	10000	1	0	1095.61 55
L1201529	001560000	10000	1	0	341.45 57
11201530	<b>001580000</b>	10000	1	0	857.24 59
11201531	001600000	0000	1	0	796.74 60
11201601	030010000	0000	1	0	905.4541 1
11201602	002010000	10000	1	0	974.2092 3
11201603	002030000	10000	1	0	388.0404 5
11201604	002050000	10000	1	Ō	1245.1044 7
		10000	1	ŏ	388.0404 9
11201605	002070000				1245.1044 11
11201606	002090000	10000	1	0	
11201607	002110000	10000	1	0	
11201608	002130000	10000	1	0	1245.1044 15
11201609	<b>002150000</b>	10000	1	0	388.0404 17
11201610	002170000	10000	1	0	1245.1044 19
11201611	002190000	10000	1	0	388.0404 21
11201612	002210000	10000	1	0	1245.1044 23
11201613	002230000	10000	1	0	388.0404 25
11201614	002250000	10000	ī	Ō	1245.1044 27
	002270000	10000	1	ŏ	388.0404 29
11201615		0000	1	õ	2489.277 31
11201616	002290000				388.0404 33
11201617	002280000	-10000	1	0	
11201618	002260000	-10000	1	0	1245.1044 35
11001619	002240000	-10000	1	0	388.0404 37
1 1620	002220000	-10000	1	0	1245.1044 39
11_J1621	002200000	-10000	1	0	388.0404 41
11201622	002180000	-10000	1	0	1245.1044 43
11201623	002160000	-10000	1	0	388.0404 45
11201624	002140000		1	0	1245.1044 47
11201625	002120000		ī	Ō	388.0404 49
	002100000		1	ŏ	1245.1044 51
11201626				ŏ	388.0404 53
11201627	002080000		1		
11201628	002060000		1		1245.1044 55
11201629	002040000		1		
11201630	002020000				974.2092 59
11201631	030010000				905.4541 60
11201701	0 0.0	0.0	0.0		60
11201801	0.0 15.0	15.0	1.5		1.5 0.0 0.0 1.0
11201901	0.0 15.0	15.0	1.5		1.5 0.0 0.0 1.0
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	ماه باو باو باو باو باو باو بار بار بار بار بار بار			++-	****
20100100				1100	UNET
20100101	70.0	2.3843€			
20100102	200.0	2.5232€			
20100103	400.0	2.80096	≥-03		
20100104	600.0	3.0787€	e-03		
2 0105	800.0	3.35656			
10106	1000.0	3.65746			
20100107	1200.0	3.98150			
	1400.0	4.30566			
20100108		55.6833			
20100151	70.0				
20100152	200.0	55.522	1		

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158/174 1+ML 10/1/96 5TA - 042 R. 0

60 60

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55.2607
20100153
             400.0
20100154
             600.0
                        54.9895
                         54.7069
20100155
             800.0
                        54.3982
    2156
            1000.0
2
                         54.0907
21. .0157
            1200.0
                        53.7516
20100158
            1400.0
    control component cards
    compute pressure difference
       *******
                ************************
                                                ******
*****
                                           0.0
                                                 1
20500100
            delptp1
                             1.45038e-4
                      sum
20500101
                                         1.0, p,
                                                  002030000
            0.0
                            002040000
                  -1.0, p,
                      sum
                                           0.0
                                                 1
            delptp2
                             1.45038e-4
20500200
                                         1.0, p,
                                                  002070000
20500201
            0.0
                  -1.0, p,
                            002080000
                             1.45038e-4
                                           0.0
                                                 1
20500300
            delptp3
                      sum
                                         1.0, p,
20500301
            0.0
                  -1.0, p,
                            002120000
                                                  002110000
                             1.45038e-4
                                           0.0
                                                 1
20500400
           delptp4
                      sum
                                         1.0, p,
                            002160000
                                                  002150000
                  -1.0, p,
20500401
            0.0
                                           0.0
                                                 1
20500500
           delptp5
                      sum
                             1.45038e-4
                            002200000
                                         1.0, p,
                                                  002190000
                  -1.0, p,
20500501
           0.0
                                           0.0
20500600
           delptp6
                      sum
                             1.45038e-4
                                                 1
                                         1.0, p,
                                                  002230000
                  -1.0, p,
                            002240000
20500601
            0.0
                                           0.0
                                                 1
20500700
           delptp7
                      sum
                             1.45038e-4
                                                  002270000
                            002280000
                                         1.0, p,
20500701
            0.0
                  -1.0, p,
    end of the input
                *************
```

159/174 1+11 191/96 577-042 K.V

 GENERAL COMPUTATION SHEET
 SHEET NO. /60 OF/74 SHEETS

 SUBJECT
 Loads on the Steam Generator Support Plats During SLB Accident

 MADE BY
 H M Lee
 DATE
 10/1/96
 CHECK BY
 L R Chang
 APPROVED BY

Appendix E

Steam Generator Design Alternation

(Westinghouse Letter NCE-85-529)

JUN 24 '96 14:53 FR (W) OPL LICENSING

P.02/06

CN-T-90-167

161/174 334 itmc 10/1/96 sta-042 R.0

NCE-85-529 From NCD ENGINEERING WIN 474-4604 ()ape September 5, 1985 Subject GENF Inputs for Models 44, 44F, 51, 51F, and F Steam Generators

M. Oshinsky - SGTD Forest Hills

J. C. Buker CC: G. V. Smith D. E. Ford M. J. Sredzienski N. J. Georges R. M. Wilson G. P. Lilly

As we discussed on the phone last week, I have prepared a list of GENF inputs for most Westinghouse Models 44, 44F, 51, 51F, and F Steam Generators. These inputs which are based on the latest information available for the plants, should be used in conjunction with the recently revised GENF code (Version 2.0).

It is recommended that these inputs should be incorporated in your GENF data bank. Inputs for Models 13, 14, 24, 27, and 33 steam generators are not yet available. Due to the geometrical differences among these models, re-programming may be required. I plan to work on them early next year and hope to have them ready before the CDC-7600 is phased out. In the meantime, inputs from the current data bank together with the previous version of GENF should be used to calculate the performance of these older model steam generators. The input data from the current data bank are not compatible with the latest version of GENF.

Please contact me if you have any questions or comments.

Kan

K. W. Chan APPROVED; Nuclear Components Eng.

D. E. Ford, Manager Nuclear Components Eng.

qdm

Attachment

Discard Date:

Τa

412 374 4011 10 814159737259 JUN 24 '96 14:53 FR (W) OPL LICENSING

372-042 R.O P.03/06 1/174

51 SERIES STEAM GENERATORS

Default Geometry:

297-000-( مار Found 

≿ :		2.2	10.50	12.01	8 X	33.64	21.50	00.53+	4.587	•.34 45.3 <b>8</b>	0.375	6.95256 51599.	854.M	
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DEFAULT GEONETRY		C III	Shid	9100	R R C	ţţ		ELEDE	DIDCI	KED NGD		28	23	
STEM COCIATOR	•	<b>3</b>	2.2 2.2	25	83.	x 3 03. 2 <b>13 1</b> 2 (		• -	969-25 969-25	88				4444444 RRRRRR
3	- JOR		2110		A T		533 233	MISTC •			X5 Trube •	 284		22222222 22222222 222222222 222222222
DATA BASED ON NODEL	5	- <b>2</b> . 		3-	56.00 22.19	5 <b>M</b> N	232.16 14.01 16.11	159.15 41.45 721.15	5. 40 9. 40 9. 40	- 14.57 1.5.6		0.258 7.00 1.2810		
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JUN 24 '96 14:54 FR (W) OPL LICENSING 412 374 4011 TO 814159737259

P.04/06 1.63/174 AMC 10/1/96 STA-042 R.D

#### 51 Series Steam Generators Standard Features:

- 3 56-inch primary separators 0
- Steam nozzle with no flow limiting devices 0
- Fillet type tube-to-tubesheat weld 0
- Secondary separator with Westinghouse formed vanes 0 and perforated plates
- Downcomer resistance plate removed 0
- 0.5 orifice 0

Farley 1 (ALA)

Special features:	None
List input update:	<b>RF = 0.00016, CKSEP2 = 125.0</b>

Farley 2 (APR)

Special features:	7 inch wrapper opening				
List input update:	HWO = 7.00, XLN = 385.81, RF = 0.00016, CKSEP2 = 125.0				

D. C. Cook 1  $\neq$  2 (AEP/AMP)

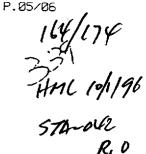
Special features:	None
List input update:	RF = 0.00020, CKSEP2 = 125.0

Zion 1 & 2 (CWE/COM)

Special features:	0.6 orifice High downcomer resistance plate setting
List input update:	DPOD = 33.50, CKDC = 16.9, CKSEP2 = 125.0

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Beaver Valley 1 (DLW

CN-T-90-

Special features: None RF = 0.00016, CKSEP2 = 125.0List input update:

TAKAHAMA 1 (TAK)

0.6 orifice Special features: Low downcomer resistance plate satting DPOD = 33.50, CKDC = 7.26, CKSEP2 = 125.0 List input update:

OHI 1 (OHI)

0.6 orifice Special features: Low downcomer resistance plate setting DPOD = 33.50, CKDC = 7.26, RF = 0.00005, List input update: CKSEP2 = 125.0

KORI 1 (KOR)

Special features:	7 inch wrapper opening
List input update:	HWO = 7.00, XLW = 385.81, CKSEP2 = 125.0

Prairie Island 1 & 2 (NSP/NRP)

Special features:	None
List input update:	RF = 0.00018, CKSEP2 = 125.0

Diablo Canvon 1 (PGE)

Special features:	None	XLW= 380.81
List input update:	RF = 0.00018,	CKSEP2 = 125.0

JUN 24 '96 14:54 FR (W) OPL LICENSING 412 374 4011 TO 814159737259

P.06/06

165/174 14ML 10/196 5TA-042 R.O

#### Diablo Canyon 2 (PEG)

Special features:	None
List input update:	RF = 0.00018, CKSEP2 = 125.0

#### Troian (POR)

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۰.

Special features:	None
List input update:	RF = 0.00005, CKSEP2 = 125.0

#### Salem 1 (PSE)

Special features:	None
List input update:	RF = 0.00018, CKSEP2 = 125.0

#### Secuovah 1 (TVA)

Special features:	None
List input update:	RF = 0.00006, CKSEP2 = 125.0

Seauovah 2 (TEN)

Special features:	None
List input update:	RF = 0.00006, CKSEP2 = 125.0

#### North Anna 1 (VRA)

Special features:	None
List input update:	RF = 0.00005, CKSEP2 = 125.0

#### 10 of 18

\*\* TOTAL PAGE.06 \*\*

#### PACIFIC GAS AND ELECTRIC COMPANY GENERAL COMPUTATION SHEET

CALC NO. STA-042 <u>*R*, b</u> SUBJECT Loads on the Steam Generator Support Plats During SLB Accident MADE BY <u>H M Lee</u> DATE 10/1/96 CHECK BY <u>L R Chang</u> APPROVED BY

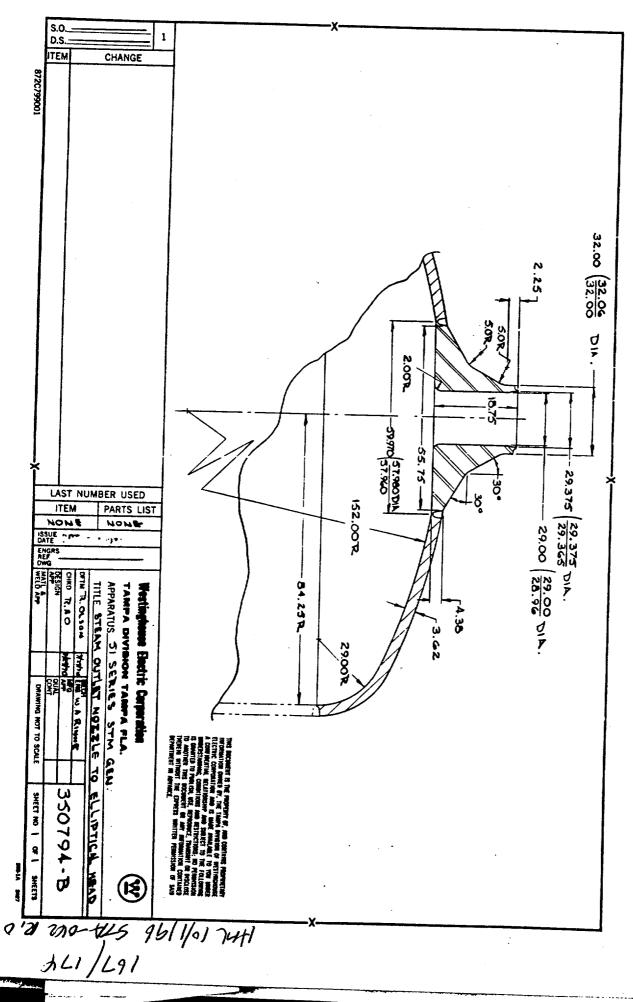
SHEET NO 166 OF / 74 SHEETS

Appendix F

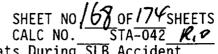
Westinghouse Drawing 350794-B

Steam Generator Nozzle to Elliptical Head

51 Series Steam Generator



- 67-



 PACIFIC GAS AND ELECTRIC COMPANY

 FNERAL COMPUTATION SHEET

 SUBJECT
 Loads on the Steam Generator Support Plats During SLB Accident

 MADE BY
 H M Lee

 DATE
 10/1/96

 CHECK BY
 L R Chang

 APPROVED BY

Appendix G

Microfiches for the RELAP5 Runs

GF "AL COMPUTATION SHEET SHEET NO. 1740F/74 SHEETS CALC NO. STA-042 R. D SUBJECT Loads on the Steam Generator Support Plats During SLB Accident MADE BY HM Lee DATE /\*/196 CHECK BY L R Chang APPROVED BY

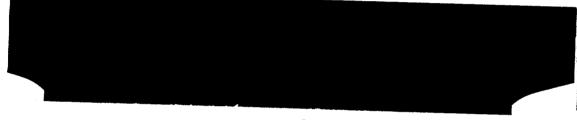


REODP 6

 ERAL COMPUTATION SHEET
 SHEET NO.173 OF/74 SHEETS CALC NO. STA-042 R. 0

 SUBJECT
 Loads on the Steam Generator Support Plats During SLB Accident

 MADE BY
 H M Lee
 DATE 10/196 CHECK BY L R Chang APPROVED BY



REODP5

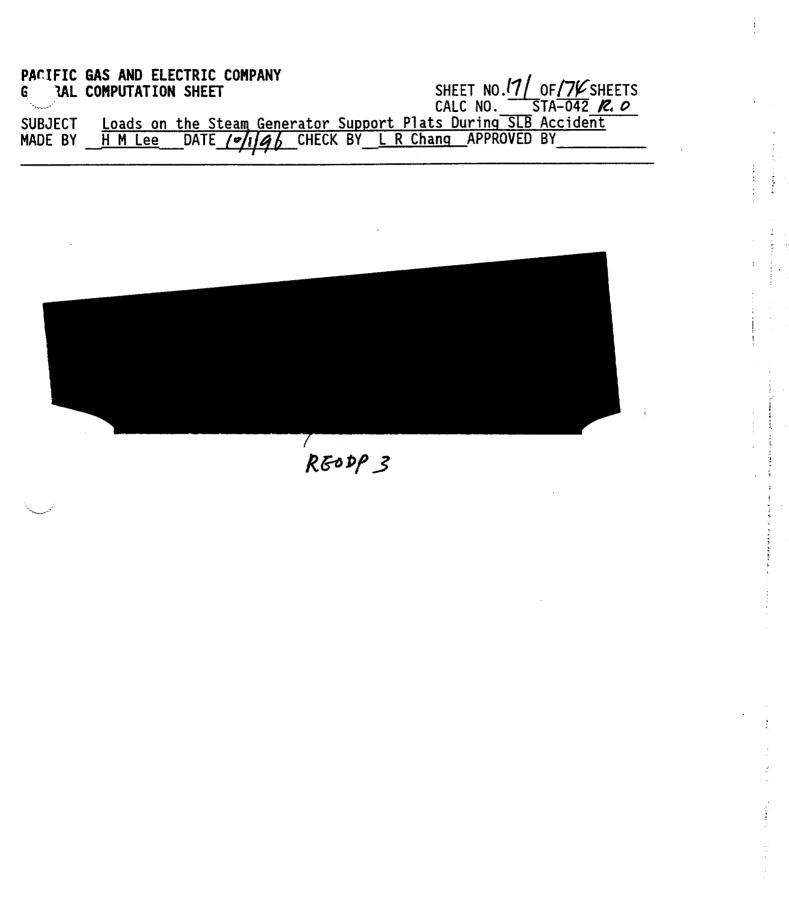
## P\*\*\*FIC GAS AND ELECTRIC COMPANY SHEET NO. 172 OF 174 SHEETS CALC NO. STA-042 R.O SUBJECT Loads on the Steam Generator Support Plats During SLB Accident MADE BY H M Lee DATE 191196 CHECK BY L R Chang APPROVED BY



RGODP 4

APPENDER PRO-

C and a set



# IFIC GAS AND ELECTRIC COMPANY GENERAL COMPUTATION SHEET SHEET NO.170 OF 174 SHEETS CALC NO. STA-042 R.P SUBJECT Loads on the Steam Generator Support Plats During SLB Accident MADE BY H M Lee DATE 10/196 CHECK BY L R Chang APPROVED BY





 IERAL COMPUTATION SHEET

 SHEET NO/64 OF /74 SHEETS CALC NO. STA-042 R.0

 SUBJECT Loads on the Steam Generator Support Plats During SLB Accident

 MADE BY
 H M Lee
 DATE /0/166 CHECK BY L R Chang APPROVED BY





#### Enclosure 3 PG&E Letter DCL-00-030

### Hard Copy Listings of Input Decks for RELAP5

```
RELAP5 Input Deck reidp1
Large Break Case 1 - No flow restrictor, non-equilibrium
=SLB pressure difference across the SG tube support plats
* hot standby nonequilibrium models
*
100 new transnt
*
102 british british
105
*
*******
*
   time step cards
*
201 5. 1.d-7 0.005 3 2 200 10000
202 5.3 1.d-7 0.00001 3 1000 20000 100000
203 6.5 1.d-7 0.000025 3 400 8000 100000
204 8.0 1.d-7 0.00005 3 200 10000 100000
205 1000.0 1.d-7 0.00010 3 100 10000 100000
   minor edit variables
*
301 mflowj 518000000
302 mflowj 002030000
303 mflowj 002070000
304 mflowj 002110000
305 mflowj 002150000
306 mflowj 002190000
307 mflowj 002230000
308 mflowj 002270000
          017010000
309 p
*310 p
           018010000
*311 p
*312 p
           019010000
           020010000
*313 p 021010000
*314 p 022010000
*315 p 023010000
*316 p 033010000
*317 p
           034010000
*318 p
           036010000
319 cntrlvar 1
320 cntrlvar 2
321 cntrivar 3
322 cntrlvar 4
323 cntrivar 5
324 cntrlvar 6
325 cntrlvar 7
*
```

```
RELAP5 Input Deck reidp1
Large Break Case 1 - No flow restrictor, non-equilibrium
*
*
******
  trip input data
*
501 time 0 ge null 0 8.0 l
502 time 0 ge null 0 5.0 l
503 time 0 ge null 0 200.0 I
600 501
*********************
  hydrodynamic components
    *********
  primary side model
  hot leg and cold leg represented by tdvs
1000000 inplen tmdpvol
1000101 0.0 10.0 5000.0 0.0 0.0 0.0 0.0 0.0 0
1000200 3
1000201 0.0 2235.7 547.0
1000202 5.0 2250.0 547.0
1000203 15.0 800.0 491.0
*1000204 1.0e6 800.0 491.0
1010000 outplen tmdpvol
1010101 0.0 10.0 5000.0 0.0 0.0 0.0 0.0 0.0 0
1010200 3
1010201 0.0 2200.0 547.0
1010202 5.0 2200.0 547.0
1010203 15.0 700.0 491.0
0010000 tubes pipe
0010001 60
0010101 10.956 60
0010301 1.1667 1
0010302 1.2553 3
0010303 0.5
          5
0010304 1.60435 7
0010305 0.5 9
```

0010306 1.60435 11

```
RELAP5 Input Deck reidp1
Large Break Case 1 - No flow restrictor, non-equilibrium
0010307 0.5
              13
0010308 1.60435 15
0010309 0.5
             17
0010310 1.60435 19
0010311 0.5
             21
0010312 1.60435 23
0010313 0.5
             25
0010314 1.60435 27
0010315 0.5
             29
0010316 3.0
              31
0010317 0.5
              33
0010318 1.60435 35
0010319 0.5
              37
0010320 1.60435 39
0010321 0.5
            41
0010322 1.60435 43
0010323 0.5
             45
0010324 1.60435 47
0010325 0.5
            49
0010326 1.60435 51
0010327 0.5
             53
0010328 1.60435 55
0010329 0.5
            57
0010330 1.2553 59
0010331 1.1667 60
0010601 90.0 30
0010602 -90.0 60
0010801 0.0 0.0642 60
0011001 00000 60
0011101 000000 59
0011201 3 2250.0 547.0 0.0 0.0 0.0 60
0011300 1
0011301 9148.5 0.0 0.0 59
5000000 prminl tmdpjun
5000101 10000000 1000000 10.956
5000200
        1
5000201 0.0 9148.5 0.0 0.0
5000202 1.0e6 9148.5 0.0 0.0
5010000 prmout tmdpjun
5010101 1010000 101000000 10.956
5010200 1
5010201 0.0 9148.5 0.0 0.0
5010202 1.0e6 9148.5 0.0 0.0
0020000 shell pipe
0020001 30
```

0020101 54.22 27

.....

<u>RELAP5 Input Deck reidp1</u> Large Break Case 1 - No flow restrictor, non-equilibrium

Large Dr	eak case I - no now i
0020102	70.0 30
0020201	54.22 2
0020202	
	54.22 6
	23.716 7
	54.22 10
0020206	23.716 11
0020207	54.22 14
	23.716 15
	54.22 18
	23.716 19
	54.22 22
	23.716 23
0020213	54.22 26
0020214	23.716 27
0020215	70.0 29
	1.2553 1
0020302	1.2553 2
0020303	
	1.60435 6
0020305	
	1.60435 10
0020307	0.5 12
0020308	1.60435 14
0020309	0.5 16
	1.60435 18
	0.5 20
	1.60435 22
0020313	0.5 24
	1.60435 26
0020314	
	3.2075 29
	3.4338 30
0020601	
0020801	0.00015 0.136 29
0020802	0.00015 0.0 30
0020901	0.0 0.0 2
0020902	0.78 0.78 3
0020903	0.0 0.0 6
0020904	
0020905	
0020905	
0020907	0.0 0.0 14
0020908	0.78 0.78 15
0020909	0.0 0.0 18
0020910	0.78 0.78 19
0020911	0.0 0.0 22
0020912	0.78 0.78 23
0020913	0.0 0.0 26
0020914	0.78 0.78 27
0020915	0.0 0.0 29
0020913	
0021001	00100 23

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Large Break Case 1	- No flow restrictor,	non-equilibrium

0004000	00000	<u></u>				
0021002		0				
0021101		29				
0021201	3 1033.73		0.0	0.0	0.0	1
0021202	3 1033.34	547.0	0.0	0.0	0.0	2
0021203	3 1033.07	547.0	0.0	0.0	0.0	3
0021204	3 1032.91	547.0	0.0	0.0	0.0	4
0021205	3 1032.57	547.0	0.0	0.0	0.0	5
0021206	3 1032.06		0.0	0.0	0.0	6
0021207	3 1031.72		0.0	0.0	0.0	7
0021208	3 1031.56		0.0	0.0	0.0	8
0021200	3 1031.22		0.0	0.0	0.0	9
0021203	3 1031.22		0.0	0.0	0.0	9 10
0021210	3 1030.71					11
			0.0	0.0	0.0	
0021212	3 1030.21		0.0	0.0	0.0	12
0021213	3 1029.87		0.0	0.0	0.0	13
0021214	3 1029.36		0.0	0.0	0.0	14
0021215	3 1029.02		0.0	0.0	0.0	15
0021216	3 1028.86		0.0	0.0	0.0	16
0021217	3 1028.53	547.0	0.0	0.0	0.0	17
0021218	3 1028.01	547.0	0.0	0.0	0.0	18
0021219	3 1027.68	547.0	0.0	0.0	0.0	19
0021220	3 1027.52	547.0	0.0	0.0	0.0	20
0021221	3 1027.18	547.0	0.0	0.0	0.0	21
0021222	3 1026.66		0.0	0.0	0.0	22
0021223	3 1026.33		0.0	0.0	0.0	23
0021224	3 1026.17		0.0	0.0	0.0	24
0021225	3 1025.83		0.0	0.0	0.0	25
0021226	3 1025.32		0.0	0.0	0.0	26
0021220	3 1023.32		0.0	0.0	0.0	20
0021227	3 1024.82		0.0			
				0.0	0.0	28
0021229	3 1024.23		0.0	0.0	0.0	29
0021230	3 1023.17	547.0	0.0	0.0	0.0	30
0021300	1		~~			
0021301	0.0 0.		29			
	0.0625	0.0 1.0	1.0	29		
*						
*						
	downc pip	е				
0350001						
0350101	0.0 3					
0350201	7.096 2					
0350301	11.827 3					
0350401	122.4 3					
0350601						
	0.00015	0.4275	3			
	00000 3		-			
	000000 2	•				
	3 1024.84		0.0	00	0.0	1
	3 1024.64					
	3 1028.04					
		547.0	0.0	0.0	0.0	3
0351300		0 0 0	2			
0351301	0.0 0.	0.0	Z			

```
RELAP5 Input Deck reidp1
Large Break Case 1 - No flow restrictor, non-equilibrium
```

```
0300000 tubesh branch
0300001 2
            1
0300101 54.22 1.1667 0. 0. 90. 1.1667 0.00015 0.136 00100
0300200 3 1034.15 547.0
0301101 035010000 03000000 7.096 0.5 0.5 000000
0302101 030010000 002000000 4.43 5.32 5.32 000000
0301201 0.0 0.0 0.0
0302201 0.0 0.0 0.0
0340000 feedrg branch
0340001 1 1
0340101 92.1 3.1097 0.0 0. -90. -3.1097 0.00015 0.0 00000
0340200 3 1022.48 547.0
0341101 034010000 035000000 7.096 0.0 0.0 000100
0341201 0.0 0.0 0.0
0230000 abovetb snglvol
0230101 49.43 4.9423 0.0 0.0 90. 4.9423 0.00015 0.0 00000
0230200 2 1022.72 0.03
5330000 abovetb sngljun
5330101 002010000 023000000 49.43 0.0 0.0 000100
5330110 0.0 0.0 1.0 1.0
5330201 1 0.0 0.0 0.0
0220000 speratr separatr
0220001 3 1
0220101 41.73 3.9156 0.0 0. 90. 3.9156 0.00015 0.0 00000
0220200 2 1021.14 1.0
0221101 022010000 021000000 12.828 0.84 0.47 000000
0222101 022000000 032000000 17.35 0.597 0.597 000000
0223101 023010000 022000000 41.73 8.689 8.689 000000
0221201 0.0 0.0 0.0
0222201 0.0 0.0 0.0
0223201 0.0 0.0 0.0
0320000 ligsept snglvol
0320101 17.35 0.0 86.75 0.0 0. 0.0 0.00015 0.0 00000
0320200 2 1021.26 0.92
0330000 abovf1 branch
0330001 2 1
0330101 100.7 2.9225 0.0 0.0 -90.0 -2.9225 0.00015 0.0 00000
0330200 2 1021.72 0.73
```

```
RELAP5 Input Deck reidp1
Large Break Case 1 - No flow restrictor, non-equilibrium
0331101 032010000 033000000 17.35 0.0 0.0 000000
0332101 033010000 034000000 79.288 0.0 0.0 000000
0331201 0.0 0.0 0.0
0332201 0.0 0.0 0.0
0530000 abovfr2 branch
0530001 2 1
0530101 100.7 3.9156 0.0 0.0 -90.0 -3.9156 0.00015 0.0 00000
0530200 2 1021.72 0.73
0531101 036010000 053000000 2.34 0.5 0.5 000000
0532101 053010000 033000000 100.7 0.0 0.0 000000
0531201 0.0 0.0 0.0
0532201 0.0 0.0 0.0
0210000 abovspr branch
0210001 2 1
0210101 152.19 2.281 0.0 0.0 90. 2.281 0.00015 0.0 00000
0210200 2 1021.12 1.0
0211101 021010000 020000000 70.75 0.0 0.0 000100
0212101 021000000 053000000 7.96 1.78 1.67 000000
0211201 0.0 0.0 0.0
0212201 0.0 0.0 0.0
0200000 spsteam snglvol
0200101 70.75 7.4502 0.0 0.0 90. 7.4502 0.00015 0.0 00000
0200200 2 1020.96 1.0
0190000 dryer separatr
0190001 3
           1
0190101 171.4 0.7083 0.0 0. 0. 0. 0.00015 0.0 00000
0190200 2 1020.96 1.0
0191101 019010000 018000000 63.49 5.502 5.502 000000
0192101 01900000 03600000 2.34 0.5 0.5 000000
0193101 020010000 019000000 70.75 0.5 0.5 000000
0191201 0.0 0.0 0.0
0192201 0.0 0.0 0.0
0193201 0.0 0.0 0.0
0360000 dsdryer snglvol
0360101 2.34 9.7312 0.0 0.0 -90. -9.7312 0.00015 0.0 00000
0360200 2 1021.57 0.82
0180000 updryer snglvol
0180101 63.49 0.0 473.0 0.0 0. 0.0 0.00015 0.0 00000
0180200 2 1020.96 1.0
```

```
RELAP5 Input Deck reidp1
Large Break Case 1 - No flow restrictor, non-equilibrium
0170000 sgdoom snglvol
0170101 94.12 3.5497 0.0 0.0 90. 3.5497 0.00015 0.0 00000
0170200 2 1020.94 1.0
0380000 contrim snglvol
0380101 10000.0 200.0 0.0 0.0 90. 200.0 0.0 0.0 00000
0380200 2 14.7 1.0
5190000 abovefr sngljun
5190101 018010000 017000000 63.49 0.0 0.0 000000
5190110 0.0 0.0 1.0 1.0
5190201 1 0.0 0.0 0.0
5180000 break valve
5180101 017010000 038000000 4.6 0.0 0.0 000100
5180110 0.0 0.0 1.0 1.0
5180201 1 0.0 0.0 0.0
5180300 mtrvlv
5180301 502 503 1000.0 0.0
* heat structure input
******
11201000 60 11 2 1 0.0321
11201100 0 2
11201101 0.000438 10
11201201 1
             10
11201301 0.0 10
11201401 547.0
                11
11201501 001010000 0000 1 0 796.74 1
11201502 001020000 10000 1 0 857.24 3
11201503 001040000 10000 1 0 341.45 5
11201504 001060000 10000 1 0 1095.61 7
11201505 001080000 10000 1 0 341.45 9
11201506 001100000 10000 1 0 1095.61 11
11201507 001120000 10000 1 0 341.45 13
11201508 001140000 10000 1 0 1095.61 15
11201509 001160000 10000 1 0 341.45 17
11201510 001180000 10000 1 0 1095.61 19
11201511 001200000 10000 1 0 341.45 21
11201512 001220000 10000 1 0 1095.61 23
11201513 001240000 10000 1 0 341.45 25
11201514 001260000 10000 1 0 1095.61 27
11201515 001280000 10000 1 0 341.45 29
11201516 001300000 10000 1 0 2190.4 31
11201517 001320000 10000 1 0 341.45 33
```

	put Deck rei ok Case 1 - N		rec	tric	tor, non-equilibrium
11201518	001340000		<u>1</u>	0	1095.61 35
11201518	001360000		1	0	341.45 37
11201519	001380000	10000	1	0	1095.61 39
11201520	001300000		1	0	341.45 41
			1		
11201522				0	1095.61 43
11201523	001440000		1	0	341.45 45
11201524	001460000		1	0	1095.61 47
11201525	001480000	10000	1	0	341.45 49
11201526	001500000	10000	1	0	1095.61 51
11201527	001520000	10000	1	0	341.45 53
11201528	001540000		1	0	1095.61 55
11201529	001560000		1	0	341.45 57
11201530	001580000	10000	1	0	857.24 59
11201531	001600000	0000	1	0	796.74 60
11201601	030010000	0000	1	0	905.4541 1
11201602	002010000		1	0	974.2092 3
11201603	002030000		1	0	388.0404 5
11201604	002050000	10000	1	0	1245.1044 7
11201605	002070000	10000	1	0	388.0404 9
11201606	002090000	10000	1	0	1245.1044 11
11201607	002110000		1	0	388.0404 13
11201608	002130000		1	0	1245.1044 15
11201609	002150000		1	0	388.0404 17
11201610	002170000	10000	1	0	1245.1044 19
11201611	002190000	10000	1	0	388.0404 21
11201612	002210000	10000	1	0	1245.1044 23
11201613	002230000		1	0	388.0404 25
11201614	002250000		1	0	1245.1044 27
11201615	002270000	10000	1	0	388.0404 29
11201616	002290000	0000	1	0	2489.277 31
11201617			1	0	388.0404 33
11201618	002260000		1	0	
11201619	002240000		1	0	
11201620	002220000		1	0	
11201621	002200000		1	0	
11201622	002180000		1	0	1245.1044 43
11201623	002160000		1	0	388.0404 45
11201624	002140000		1	0	1245.1044 47
11201625	002120000		1	0	388.0404 49
11201626	002100000		1	0	
11201627	002080000	-10000	1	0	388.0404 53
11201628	002060000	-10000	1	0	1245.1044 55
11201629	002040000	-10000	1	0	
11201630	002020000	-10000	1	0	974.2092 59
11201631	030010000	0000	1	0	905.4541 60
11201701	0 0.0 0.0	0.0	6	0	
11201801	0.0 15.0 1	5.0 1.5	5	1.5	0.0 0.0 1.0 60
11201901	0.0 15.0 1	5.0 1.5	5	1.5	0.0 0.0 1.0 60
*					
*					

\* composition type and data format

Large Break Case 1 - No flow restrictor, non-equilibrium

~~~~~~~	~~~~~~	~~~~~~
20100100	tbl/fctn	1 1 * inconel
20100101		2.3843e-03
20100102	200.0	2.5232e-03
20100103	400.0	2.8009e-03
20100104		
20100105		3.3565e-03
20100106		3.6574e-03
20100107		3.9815e-03
20100108	1400.0	4.3056e-03
20100151		55.6831
20100152		
20100153		
20100154		
20100155		
20100156	1000.0	54.3982
20100157		54.0907
20100158 *	1400.0	53.7516
* control o	componer	nt cards
*	•	
* compute	e pressure	e difference
******	******	*****
20500100	delptp1	sum 1.45038e-4 0.0 1
20500101		0, p, 002040000 1.0, p, 002030000
20500200		sum 1.45038e-4 0.0 1
20500201	0.0 -1.0	0, p, 002080000 1.0, p, 002070000
20500300		sum 1.45038e-4 0.0 1
20500301	0.0 -1.0	0, p, 002120000 1.0, p, 002110000
20500400	delptp4	sum 1.45038e-4 0.0 1
20500401	0.0 -1.0	0, p, 002160000 1.0, p, 002150000
20500500	delptp5	sum 1.45038e-4 0.0 1
20500501	0.0 -1.0	0, p, 002200000 1.0, p, 002190000
		sum 1.45038e-4 0.0 1
		0, p, 002240000 1.0, p, 002230000
		sum 1.45038e-4 0.0 1
20500701 *	0.0 -1.0	0, p, 002280000 1.0, p, 002270000
* end of th	ne input	
*	1	
***********	********	******

```
RELAP5 Input Deck reidp2
Large Break Case 2 - No flow restrictor, equilibrium
=SLB pressure difference across the SG tube support plats
* hot standby nonequilibrium models
100 new transnt
102 british british
105
*
*******
   time step cards
201
     5. 1.d-7 0.005 3 2
                            200
                                  10000
202 5.3 1.d-7 0.00001 3 1000 20000 100000
203 6.5 1.d-7 0.000025 3 400 8000 100000
204 8.0 1.d-7 0.00005 3 200 10000 100000
205 1000.0 1.d-7 0.00010 3 100 10000 100000
                   *****
   minor edit variables
*
301 mflowj 518000000
302 mflowj 002030000
303 mflowj 002070000
304 mflowj 002110000
305 mflowj 002150000
306 mflowj 002190000
307 mflowj 002230000
308 mflowj 002270000
309 p
          017010000
*310 p
          018010000
*311 p
          019010000
*312 p
          020010000
*313 p
          021010000
*314 p
          022010000
*315 p
          023010000
*316 p
          033010000
*317 p
          034010000
*318 p
          036010000
319 cntrlvar 1
320 cntrlvar 2
321 cntrlvar 3
322 cntrlvar 4
323 cntrlvar 5
324 cntrlvar 6
325 cntrlvar 7
```

Large Break Case 2 - No flow restrictor, equilibrium \* \*\*\*\*\* trip input data \* \* 501 time 0 ge null 0 8.0 l 502 time 0 ge null 0 5.0 l 503 time 0 ge null 0 200.0 I \* 600 501 \*\*\*\*\* hydrodynamic components \*\*\*\*\*\*\* primary side model hot leg and cold leg represented by tdvs 1000000 inplen tmdpvol 1000101 0.0 10.0 5000.0 0.0 0.0 0.0 0.0 0.0 0 1000200 3 1000201 0.0 2235.7 547.0 1000202 5.0 2250.0 547.0 1000203 15.0 800.0 491.0 \*1000204 1.0e6 800.0 491.0 \* 1010000 outplen tmdpvol 1010101 0.0 10.0 5000.0 0.0 0.0 0.0 0.0 0.0 0 1010200 3 1010201 0.0 2200.0 547.0 1010202 5.0 2200.0 547.0 1010203 15.0 700.0 491.0 0010000 tubes pipe 0010001 60 0010101 10.956 60 0010301 1.1667 1 0010302 1.2553 3 0010303 0.5 5 0010304 1.60435 7 0010305 0.5 9

0010306 1.60435 11

```
RELAP5 Input Deck reidp2
Large Break Case 2 - No flow restrictor, equilibrium
0010307 0.5
             13
0010308 1.60435 15
0010309 0.5
             17
0010310 1.60435 19
0010311 0.5
             21
0010312 1.60435 23
0010313 0.5
             25
0010314 1.60435 27
0010315 0.5
             29
0010316 3.0
             31
0010317 0.5
             33
0010318 1.60435 35
0010319 0.5
             37
0010320 1.60435 39
0010321 0.5 41
0010322 1.60435 43
0010323 0.5
            45
0010324 1.60435 47
0010325 0.5 49
0010326 1.60435 51
0010327 0.5
            53
0010328 1.60435 55
0010329 0.5 57
0010330 1.2553 59
0010331 1.1667 60
0010601 90.0 30
0010602 -90.0 60
0010801 0.0 0.0642 60
0011001 00000 60
0011101 000000 59
0011201 3 2250.0 547.0 0.0 0.0 0.0 60
0011300 1
0011301 9148.5 0.0 0.0 59
500000 prminl tmdpjun
5000101 10000000 1000000 10.956
5000200 1
5000201 0.0 9148.5 0.0 0.0
5000202 1.0e6 9148.5 0.0 0.0
5010000 prmout tmdpjun
5010101 1010000 101000000 10.956
5010200 1
5010201 0.0 9148.5 0.0 0.0
5010202 1.0e6 9148.5 0.0 0.0
0020000 shell pipe
0020001 30
0020101 54.22 27
```

Large Break Case 2 - No flow restrictor, equilibrium

<u>RELAP5 Input Deck reidp2</u> Large Break Case 2 - No flow restrictor, equilibrium

0021002	00001 30	
0021101	000000 29	
0021201	3 1033.73 547.0 0.0 0.0 0.0 1	
0021202	3 1033.34 547.0 0.0 0.0 0.0 2	
0021203	3 1033.07 547.0 0.0 0.0 0.0 3	
0021204	3 1032.91 547.0 0.0 0.0 0.0 4	
0021205	3 1032.57 547.0 0.0 0.0 0.0 5	
0021206	3 1032.06 547.0 0.0 0.0 0.0 6	
0021207	3 1031.72 547.0 0.0 0.0 0.0 7	
0021208	3 1031.56 547.0 0.0 0.0 0.0 8	
0021209	3 1031.22 547.0 0.0 0.0 0.0 9	
0021210	3 1030.71 547.0 0.0 0.0 0.0 10	
0021211	3 1030.37 547.0 0.0 0.0 0.0 11	
0021212	3 1030.21 547.0 0.0 0.0 0.0 12	
0021213	3 1029.87 547.0 0.0 0.0 0.0 13	
0021214	3 1029.36 547.0 0.0 0.0 0.0 14	
0021215	3 1029.02 547.0 0.0 0.0 0.0 15	
0021216	3 1028.86 547.0 0.0 0.0 0.0 16	
0021217	3 1028.53 547.0 0.0 0.0 0.0 17	
0021218	3 1028.01 547.0 0.0 0.0 0.0 18	
0021219	3 1027.68 547.0 0.0 0.0 0.0 19	
0021220	3 1027.52 547.0 0.0 0.0 0.0 20	
0021221	3 1027.18 547.0 0.0 0.0 0.0 21	
0021222	3 1026.66 547.0 0.0 0.0 0.0 22	
0021223	3 1026.33 547.0 0.0 0.0 0.0 23	
0021224	3 1026.17 547.0 0.0 0.0 0.0 24	
0021225	3 1025.83 547.0 0.0 0.0 0.0 25	
0021226	3 1025.32 547.0 0.0 0.0 0.0 26	
0021227	3 1024.98 547.0 0.0 0.0 0.0 27	
0021228	3 1024.82 547.0 0.0 0.0 0.0 28	
0021229	3 1024.23 547.0 0.0 0.0 0.0 29	
0021230	3 1023.17 547.0 0.0 0.0 0.0 30	
0021300	1	
0021301	0.0 0.0 0.0 29	
0021401	0.0625 0.0 1.0 1.0 29	
*		
*		
0350000	downc pipe	
0350001		
0350101	0.0 3	
0350201		
0350301	11.827 3	
	122.4 3	
0350601		
0350801	0.00015 0.4275 3	
0351001	00000 3	
	000000 2	
	3 1024.84 547.0 0.0 0.0 0.0 1	
	3 1028.64 547.0 0.0 0.0 0.0 2	
	3 1032.44 547.0 0.0 0.0 0.0 3	
0351300		
0351301		
	—	

## <u>RELAP5 Input Deck reidp2</u> Large Break Case 2 - No flow restrictor, equilibrium

```
0300000 tubesh branch
0300001 2
            1
0300101 54.22 1.1667 0. 0. 90. 1.1667 0.00015 0.136 00100
0300200 3 1034.15 547.0
0301101 035010000 03000000 7.096 0.5 0.5 000000
0302101 030010000 002000000 4.43 5.32 5.32 000000
0301201 0.0 0.0 0.0
0302201 0.0 0.0 0.0
0340000 feedrg branch
0340001 1
            1
0340101 92.1 3.1097 0.0 0. -90. -3.1097 0.00015 0.0 00000
0340200 3 1022.48 547.0
0341101 034010000 035000000 7.096 0.0 0.0 000100
0341201 0.0 0.0 0.0
0230000 abovetb snglvol
0230101 49.43 4.9423 0.0 0.0 90. 4.9423 0.00015 0.0 00000
0230200 2 1022.72 0.03
5330000 abovetb sngljun
5330101 002010000 023000000 49.43 0.0 0.0 000100
5330110 0.0 0.0 1.0 1.0
5330201 1 0.0 0.0 0.0
0220000 speratr separatr
0220001 3 1
0220101 41.73 3.9156 0.0 0. 90. 3.9156 0.00015 0.0 00000
0220200 2 1021.14 1.0
0221101 022010000 021000000 12.828 0.84 0.47 000000
0222101 022000000 032000000 17.35 0.597 0.597 000000
0223101 023010000 022000000 41.73 8.689 8.689 000000
0221201 0.0 0.0 0.0
0222201 0.0 0.0 0.0
0223201 0.0 0.0 0.0
0320000 ligsept snglvol
0320101 17.35 0.0 86.75 0.0 0. 0.0 0.00015 0.0 00000
0320200 2 1021.26 0.92
0330000 abovf1 branch
0330001 2 1
0330101 100.7 2.9225 0.0 0.0 -90.0 -2.9225 0.00015 0.0 00000
0330200 2 1021.72 0.73
```

```
RELAP5 Input Deck reidp2
Large Break Case 2 - No flow restrictor, equilibrium
0331101 032010000 033000000 17.35 0.0 0.0 000000
0332101 033010000 034000000 79.288 0.0 0.0 000000
0331201 0.0 0.0 0.0
0332201 0.0 0.0 0.0
0530000 abovfr2 branch
0530001 2 1
0530101 100.7 3.9156 0.0 0.0 -90.0 -3.9156 0.00015 0.0 00000
0530200 2 1021.72 0.73
0531101 036010000 053000000 2.34 0.5 0.5 000000
0532101 053010000 033000000 100.7 0.0 0.0 000000
0531201 0.0 0.0 0.0
0532201 0.0 0.0 0.0
0210000 abovspr branch
0210001 2 1
0210101 152.19 2.281 0.0 0.0 90. 2.281 0.00015 0.0 00000
0210200 2 1021.12 1.0
0211101 021010000 020000000 70.75 0.0 0.0 000100
0212101 021000000 053000000 7.96 1.78 1.67 000000
0211201 0.0 0.0 0.0
0212201 0.0 0.0 0.0
0200000 spsteam snglvol
0200101 70.75 7.4502 0.0 0.0 90. 7.4502 0.00015 0.0 00000
0200200 2 1020.96 1.0
0190000 dryer separatr
0190001 3
            1
0190101 171.4 0.7083 0.0 0. 0. 0. 0.00015 0.0 00000
0190200 2 1020.96 1.0
0191101 019010000 018000000 63.49 5.502 5.502 000000
0192101 01900000 03600000 2.34 0.5 0.5 000000
0193101 020010000 019000000 70.75 0.5 0.5 000000
0191201 0.0 0.0 0.0
0192201 0.0 0.0 0.0
0193201 0.0 0.0 0.0
0360000 dsdryer snglvol
0360101 2.34
             9.7312 0.0 0.0 -90. -9.7312 0.00015 0.0 00000
0360200 2
            1021.57 0.82
0180000 updryer snglvol
0180101 63.49 0.0 473.0 0.0 0. 0.0 0.00015 0.0 00000
0180200 2 1020.96 1.0
```

```
RELAP5 Input Deck reidp2
Large Break Case 2 - No flow restrictor, equilibrium
0170000 sgdoom snglvol
0170101 94.12 3.5497 0.0 0.0 90. 3.5497 0.00015 0.0 00000
0170200 2 1020.94 1.0
0380000 contrm snglvol
0380101 10000.0 200.0 0.0 0.0 90. 200.0 0.0 0.0 00000
0380200 2 14.7 1.0
5190000 abovefr sngljun
5190101 018010000 017000000 63.49 0.0 0.0 000000
5190110 0.0 0.0 1.0 1.0
5190201 1 0.0 0.0 0.0
5180000 break valve
5180101 017010000 038000000 4.6 0.0 0.0 000100
5180110 0.0 0.0 1.0 1.0
5180201 1 0.0 0.0 0.0
5180300 mtrvlv
5180301 502 503 1000.0 0.0
* heat structure input
******
11201000 60 11 2 1 0.0321
11201100 0 2
11201101 0.000438 10
11201201 1
             10
11201301 0.0 10
11201401 547.0
                11
11201501 001010000 0000 1 0 796.74 1
11201502 001020000 10000 1 0 857.24 3
11201503 001040000 10000 1 0 341.45 5
11201504 001060000 10000 1 0 1095.61 7
11201505 001080000 10000 1 0 341.45 9
11201506 001100000 10000 1 0 1095.61 11
11201507 001120000 10000 1 0 341.45 13
11201508 001140000 10000 1 0 1095.61 15
11201509 001160000 10000 1 0 341.45 17
11201510 001180000 10000 1 0 1095.61 19
11201511 001200000 10000 1 0 341.45 21
11201512 001220000 10000 1 0 1095.61 23
11201513 001240000 10000 1 0 341.45 25
11201514 001260000 10000 1 0 1095.61 27
11201515 001280000 10000 1 0 341.45 29
11201516 001300000 10000 1 0 2190.4 31
11201517 001320000 10000 1 0 341.45 33
```

\_

	PUT DECK FEI			tria	tor oquilibrium
					tor, equilibrium
11201518	001340000		1	0	1095.61 35
11201519	001360000	10000	1	0	341.45 37
11201520	001380000	10000	1	0	1095.61 39
11201521	001400000		1	0	341.45 41
11201522	001420000		1	0	1095.61 43
11201523	001440000		1	0	341.45 45
11201524	001460000	10000	1	0	1095.61 47
11201525	001480000	10000	1	0	341.45 49
11201526	001500000	10000	1	0	1095.61 51
11201527	001520000	10000	1	0	341.45 53
11201528	001540000	10000	1	0	1095.61 55
11201529	001560000	10000	1	0	341.45 57
11201530	001580000	10000	1	0	857.24 59
11201531	001600000	0000	1	0	796.74 60
11201601	030010000	0000	1	0	905.4541 1
11201602	002010000		1	0	974.2092 3
11201603	002030000	10000	1	0	388.0404 5
11201604	002050000	10000	1	0	1245.1044 7
11201605	002070000	10000	1	0	388.0404 9
11201606	002090000	10000	1	0	1245.1044 11
11201607	002110000	10000	1	0	388.0404 13
11201608	002130000		1	0	1245.1044 15
11201609	002150000	10000	1	0	388.0404 17
11201610	002170000	10000	1	0	1245.1044 19
11201611	002190000	10000	1	0	388.0404 21
11201612	002210000		1	0	1245.1044 23
11201613	002230000		1	0	388.0404 25
11201614	002250000	10000	1	0	1245.1044 27
11201615	002270000	10000	1	0	388.0404 29
11201616	002290000	0000	1	0	2489.277 31
11201617	002280000		1	0	388.0404 33
11201618	002260000		1	0	1245.1044 35
11201619	002240000		1	0	388.0404 37
11201620	002220000		1	0	
11201621	002200000		1	0	
11201622	002180000		1	0	1245.1044 43
11201623	002160000		1	0	388.0404 45
11201624	002140000		1	0	1245.1044 47
11201625	002120000		1	0	388.0404 49
11201626	002100000		1	0	
11201627	002080000		1	0	388.0404 53
11201628	002060000	-10000	1	0	1245.1044 55
11201629	002040000	-10000	1	0	388.0404 57
11201630	002020000	-10000	1	0	974.2092 59
11201631	030010000	0000	1	0	905.4541 60
11201701	0 0.0 0.0	0.0	6	0	
11201801	0.0 15.0 1	5.0 1.5	5	1.5	0.0 0.0 1.0 60
11201901	0.0 15.0 1	5.0 1.5	5	1.5	0.0 0.0 1.0 60
*					
*					

\* composition type and data format

RELAP5 Input Deck reidp2 Large Break Case 2 - No flow restrictor, equilibrium

		******
20100100	tbl/fctn	1 1 * inconel
20100101		
20100102		2.5232e-03
20100103		2.8009e-03
20100104		3.0787e-03
		3.3565e-03
20100106		3.6574e-03
20100107	1200.0	3.9815e-03
20100108	1400.0	4.3056e-03
20100151		
20100152		55.5227
20100153		
20100154		
20100155		
20100156		
20100157 20100158		54.0907 53.7516
20100156	1400.0	53.7510
* control c	omponer	at cards
*	omponer	
* compute	pressure	e difference
*	pressure	
*******	******	*****
20500100	delptp1	sum 1.45038e-4 0.0 1
20500101	• •	0, p, 002040000 1.0, p, 002030000
20500200		sum 1.45038e-4 0.0 1
20500201	0.0 -1.0	0, p, 002080000 1.0, p, 002070000
20500300	delptp3	sum 1.45038e-4 0.0 1
20500301	0.0 -1.0	D, p, 002120000 1.0, p, 002110000
20500400	delptp4	sum 1.45038e-4 0.0 1
20500401		D, p, 002160000 1.0, p, 002150000
20500500		sum 1.45038e-4 0.0 1
20500501		0, p, 002200000 1.0, p, 002190000
		sum 1.45038e-4 0.0 1
		0, p, 002240000 1.0, p, 002230000
		sum 1.45038e-4 0.0 1
20500701	0.0 -1.0	0, p, 002280000 1.0, p, 002270000
* end of th	a input	
*	ie input	
******	********	******

```
RELAP5 Input Deck reidp3
Small Break Case 1 - Flow restrictor, non-equilibrium
=SLB pressure difference across the SG tube support plats
* hot standby nonequilibrium models
100 new transnt
102 british british
105
*
******
   time step cards
*
201 5. 1.d-7 0.005 3 2 200 10000
202 5.3 1.d-7 0.00001 3 1000 20000 100000
203 6.5 1.d-7 0.000025 3 400 8000 100000
204 8.0 1.d-7 0.00005 3 200 10000 100000
205 1000.0 1.d-7 0.00010 3 100 10000 100000
   minor edit variables
301 mflowj 518000000
302 mflowj 002030000
303 mflowj 002070000
304 mflowj 002110000
305 mflowj 002150000
306 mflowj 002190000
307 mflowj 002230000
308 mflowj 002270000
309 p
          017010000
*310 p
           018010000
*311 p
*311 p
*312 p
           019010000
           020010000
*313 p 021010000
*314 p 022010000
*315 p
*316 p
           023010000
           033010000
*317 p
           034010000
*318 p
           036010000
319 cntrlvar 1
320 cntrlvar 2
321 cntrlvar 3
322 cntrlvar 4
323 cntrlvar 5
324 cntrlvar 6
325 cntrlvar 7
```

## <u>RELAP5 Input Deck reidp3</u> Small Break Case 1 - Flow restrictor, non-equilibrium

```
*
*****
*
  trip input data
*
*
501 time 0 ge null 0 8.0 l
502 time 0 ge null 0 5.0 l
503 time 0 ge null 0 200.0 l
600 501
    ***************
 hydrodynamic components
   primary side model
* hot leg and cold leg represented by tdvs
1000000 inplen tmdpvol
1000101 0.0 10.0 5000.0 0.0 0.0 0.0 0.0 0.0 0
1000200 3
1000201 0.0 2235.7 547.0
1000202 5.0 2250.0 547.0
1000203 15.0 800.0 491.0
*1000204 1.0e6 800.0 491.0
*
1010000 outplen tmdpvol
1010101 0.0 10.0 5000.0 0.0 0.0 0.0 0.0 0.0 0
1010200 3
1010201 0.0 2200.0 547.0
1010202 5.0 2200.0 547.0
1010203 15.0 700.0 491.0
0010000 tubes pipe
0010001 60
0010101 10.956 60
0010301 1.1667 1
0010302 1.2553 3
0010303 0.5 5
0010304 1.60435 7
0010305 0.5 9
```

0010306 1.60435 11

```
2 of 10
```

```
RELAP5 Input Deck reidp3
Small Break Case 1 - Flow restrictor, non-equilibrium
0010307 0.5
              13
0010308 1.60435 15
0010309 0.5
            17
0010310 1.60435 19
0010311 0.5
              21
0010312 1.60435 23
0010313 0.5
              25
0010314 1.60435 27
0010315 0.5
             29
0010316 3.0
              31
0010317 0.5
              33
0010318 1.60435 35
0010319 0.5
              37
0010320 1.60435 39
0010321 0.5 41
0010322 1.60435 43
0010323 0.5
            45
0010324 1.60435 47
0010325 0.5
            49
0010326 1.60435 51
0010327 0.5
             53
0010328 1.60435 55
0010329 0.5
            57
0010330 1.2553 59
0010331 1.1667 60
0010601 90.0 30
0010602 -90.0 60
0010801 0.0 0.0642 60
0011001 00000 60
0011101 000000 59
0011201 3 2250.0 547.0 0.0 0.0 0.0 60
0011300 1
0011301 9148.5 0.0 0.0 59
5000000 prminl tmdpjun
5000101 10000000 1000000 10.956
5000200 1
5000201 0.0 9148.5 0.0 0.0
5000202 1.0e6 9148.5 0.0 0.0
5010000 prmout tmdpjun
5010101 1010000 101000000 10.956
5010200 1
5010201 0.0 9148.5 0.0 0.0
5010202 1.0e6 9148.5 0.0 0.0
0020000 shell pipe
0020001 30
0020101 54.22 27
```

<u>RELAP5 Input Deck reidp3</u> Small Break Case 1 - Flow restrictor, non-equilibrium

Small Dr	eak case 1 - Flow res
0020102	
0020201	54.22 2
0020202	
	54.22 6
	23.716 7
	54.22 10
0020206	23.716 11
0020207	54.22 14
	23.716 15
	54.22 18
	23.716 19
	54.22 22
	23.716 23
0020213	54.22 26
0020214	23.716 27
0020215	70.0 29
	1.2553 1
0020302	1.2553 2
0020002	0.5 4
0020303	
	1.60435 6
0020305	
0020306	1.60435 10
0020307	0.5 12
0020308	1.60435 14
0020309	0.5 16
	1.60435 18
	0.5 20
0020313	1.60435 22 0.5 24
0020314	1.60435 26
0020314	
	3.2075 29
	3.4338 30
0020601	
0020801	0.00015 0.136 29
0020802	0.00015 0.0 30
0020901	0.0 0.0 2
0020902	0.78 0.78 3
0020903	0.0 0.0 6
0020904	0.78 0.78 7
0020905	0.0 0.0 10
0020905	
0020907	0.0 0.0 14
0020908	0.78 0.78 15
0020909	0.0 0.0 18
0020910	0.78 0.78 19
0020911	0.0 0.0 22
0020912	0.78 0.78 23
0020913	0.0 0.0 26
0020914	0.78 0.78 27
0020915	0.0 0.0 29
0020915	
0021001	00100 29

RELAP5 Input Deck reidp3 Small Break Case 1 - Flow restrictor, non-equilibrium

0021002	00000 30	
0021101	000000 29	
0021201	3 1033.73 547.0 0.0 0.0 0.0 1	
0021202	3 1033.34 547.0 0.0 0.0 0.0 2	
0021203	3 1033.07 547.0 0.0 0.0 0.0 3	
0021204	3 1032.91 547.0 0.0 0.0 0.0 4	
0021205 0021206	3 1032.57 547.0 0.0 0.0 0.0 5 3 1032.06 547.0 0.0 0.0 0.0 6	
0021208	3 1031.72 547.0 0.0 0.0 0.0 0.0 7	
0021207	3 1031.56 547.0 0.0 0.0 0.0 0.0 8	
0021209	3 1031.22 547.0 0.0 0.0 0.0 9	
0021210		0
0021211	3 1030.37 547.0 0.0 0.0 0.0 1	11
0021212	3 1030.21 547.0 0.0 0.0 0.0 1	2
0021213		3
0021214		4
0021215		5
0021216 0021217		16
0021217		7  8
0021210		19
0021220		20
0021221		21
0021222		22
0021223		23
0021224		24
0021225		25
0021226		26
0021227		27
0021228		28 29
0021220		30
0021300	1	
0021301	0.0 0.0 0.0 29	
0021401	0.0625 0.0 1.0 1.0 29	
*		
*		
	downc pipe	
0350001 0350101		
0350201		
0350301		
0350401		
0350601		
	0.00015 0.4275 3	
0351001	00000 3	
	000000 2	
0351201		
0351202		
0351203		5
0351300 0351301		
0001001	0.0 0.0 0.0 2	

## <u>RELAP5 Input Deck reidp3</u> Small Break Case 1 - Flow restrictor, non-equilibrium

```
0300000 tubesh branch
0300001 2
           1
0300101 54.22 1.1667 0. 0. 90. 1.1667 0.00015 0.136 00100
0300200 3 1034.15 547.0
0301101 035010000 03000000 7.096 0.5 0.5 000000
0302101 030010000 002000000 4.43 5.32 5.32 000000
0301201 0.0 0.0 0.0
0302201 0.0 0.0 0.0
0340000 feedrg branch
0340001 1
            1
0340101 92.1 3.1097 0.0 0. -90. -3.1097 0.00015 0.0 00000
0340200 3 1022.48 547.0
0341101 034010000 035000000 7.096 0.0 0.0 000100
0341201 0.0 0.0 0.0
0230000 abovetb snglvol
0230101 49.43 4.9423 0.0 0.0 90. 4.9423 0.00015 0.0 00000
0230200 2 1022.72 0.03
5330000 abovetb sngljun
5330101 002010000 023000000 49.43 0.0 0.0 000100
5330110 0.0 0.0 1.0 1.0
5330201 1 0.0 0.0 0.0
0220000 speratr separatr
0220001 3 1
0220101 41.73 3.9156 0.0 0. 90. 3.9156 0.00015 0.0 00000
0220200 2 1021.14 1.0
0221101 022010000 021000000 12.828 0.84 0.47 000000
0222101 022000000 032000000 17.35 0.597 0.597 000000
0223101 023010000 022000000 41.73 8.689 8.689 000000
0221201 0.0 0.0 0.0
0222201 0.0 0.0 0.0
0223201 0.0 0.0 0.0
0320000 liqsept snglvol
0320101 17.35 0.0 86.75 0.0 0. 0.0 0.00015 0.0 00000
0320200 2 1021.26 0.92
0330000 abovf1 branch
0330001 2 1
0330101 100.7 2.9225 0.0 0.0 -90.0 -2.9225 0.00015 0.0 00000
0330200 2 1021.72 0.73
```

```
RELAP5 Input Deck reidp3
Small Break Case 1 - Flow restrictor, non-equilibrium
0331101 032010000 033000000 17.35 0.0 0.0 000000
0332101 033010000 034000000 79.288 0.0 0.0 000000
0331201 0.0 0.0 0.0
0332201 0.0 0.0 0.0
0530000 abovfr2 branch
0530001 2 1
0530101 100.7 3.9156 0.0 0.0 -90.0 -3.9156 0.00015 0.0 00000
0530200 2 1021.72 0.73
0531101 036010000 053000000 2.34 0.5 0.5 000000
0532101 053010000 033000000 100.7 0.0 0.0 000000
0531201 0.0 0.0 0.0
0532201 0.0 0.0 0.0
0210000 abovspr branch
0210001 2 1
0210101 152.19 2.281 0.0 0.0 90. 2.281 0.00015 0.0 00000
0210200 2 1021.12 1.0
0211101 021010000 020000000 70.75 0.0 0.0 000100
0212101 021000000 053000000 7.96 1.78 1.67 000000
0211201 0.0 0.0 0.0
0212201 0.0 0.0 0.0
0200000 spsteam snalvol
0200101 70.75 7.4502 0.0 0.0 90. 7.4502 0.00015 0.0 00000
0200200 2 1020.96 1.0
0190000 dryer separatr
0190001 3 1
0190101 171.4 0.7083 0.0 0. 0. 0. 0.00015 0.0 00000
0190200 2 1020.96 1.0
0191101 019010000 018000000 63.49 5.502 5.502 000000
0192101 01900000 03600000 2.34 0.5 0.5 000000
0193101 020010000 019000000 70.75 0.5 0.5 000000
0191201 0.0 0.0 0.0
0192201 0.0 0.0 0.0
0193201 0.0 0.0 0.0
0360000 dsdryer snglvol
0360101 2.34 9.7312 0.0 0.0 -90. -9.7312 0.00015 0.0 00000
0360200 2 1021.57 0.82
0180000 updryer snglvol
0180101 63.49 0.0 473.0 0.0 0. 0.0 0.00015 0.0 00000
0180200 2 1020.96 1.0
```

```
RELAP5 Input Deck reidp3
Small Break Case 1 - Flow restrictor, non-equilibrium
0170000 sgdoom snglvol
0170101 94.12 3.5497 0.0 0.0 90. 3.5497 0.00015 0.0 00000
0170200 2 1020.94 1.0
0380000 contnm snglvol
0380101 10000.0 200.0 0.0 0.0 90. 200.0 0.0 0.0 00000
0380200 2 14.7
                  1.0
5190000 abovefr sngljun
5190101 018010000 017000000 63.49 0.0 0.0 000000
5190110 0.0 0.0 1.0 1.0
5190201 1 0.0 0.0 0.0
5180000 break
             valve
5180101 017010000 038000000 1.388 0.0 0.0 000100
5180110 0.0 0.0 1.0 1.0
5180201 1 0.0 0.0 0.0
5180300 mtrvlv
5180301 502 503 1000.0 0.0
* heat structure input
*****
11201000 60 11 2 1 0.0321
11201100 0
             2
11201101 0.000438
                    10
11201201 1
             10
11201301 0.0 10
11201401 547.0
                11
11201501 001010000 0000 1 0 796.74 1
11201502 001020000 10000 1 0 857.24 3
11201503 001040000 10000 1 0 341.45 5
11201504 001060000 10000 1 0 1095.61 7
11201505 001080000 10000 1 0 341.45 9
11201506 001100000 10000 1 0 1095.61 11
11201507 001120000 10000 1 0 341.45 13
11201508 001140000 10000 1 0 1095.61 15
11201509 001160000 10000 1 0 341.45 17
11201510 001180000 10000 1 0 1095.61 19
         001200000 10000 1 0 341.45 21
11201511
11201512 001220000 10000 1 0 1095.61 23
11201513 001240000 10000 1 0 341.45 25
11201514 001260000 10000 1 0 1095.61 27
11201515 001280000 10000 1 0 341.45 29
11201516 001300000 10000 1 0 2190.4 31
11201517 001320000 10000 1 0 341.45 33
```

	k Case 1 - F		trid	ctor	<u>, non-equilibrium</u>
<u>11201518</u>	001340000		1	0	1095.61 35
11201510	001360000	10000	1	Ő	341.45 37
11201520	001380000	10000	1	Ő	1095.61 39
11201521	001400000		1	Ő	341.45 41
11201522	001420000		1	Ő	1095.61 43
11201523	001440000		1	Ő	341.45 45
11201524	001460000		1	õ	1095.61 47
11201525	001480000	10000	1	õ	341.45 49
11201526	001500000	10000	1	õ	1095.61 51
11201527	001520000	10000	1	Ō	341.45 53
11201528	001540000	10000	1	0	1095.61 55
11201529	001560000	10000	1	0	341.45 57
11201530	001580000	10000	1	0	857.24 59
11201531	001600000	0000	1	0	796.74 60
11201601	030010000		1	0	905.4541 1
11201602	002010000		1	0	974.2092 3
11201603	002030000	10000	1	0	388.0404 5
11201604	002050000	10000	1	0	1245.1044 7
11201605	002070000	10000	1	0	388.0404 9
11201606	002090000	10000	1	0	1245.1044 11
11201607	002110000	10000	1	0	388.0404 13
11201608	002130000	10000	1	0	1245.1044 15
11201609	002150000	10000	1	0	388.0404 17
11201610	002170000	10000	1	0	1245.1044 19
11201611	002190000	10000	1	0	388.0404 21
11201612	002210000	10000	1	0	1245.1044 23
11201613	002230000	10000	1	0	388.0404 25
11201614	002250000	10000	1	0	1245.1044 27
11201615	002270000	10000	1	0	388.0404 29
11201616	002290000	0000	1	0	2489.277 31
11201617	002280000		1	0	
11201618	002260000		1	0	1245.1044 35
11201619	002240000		1		
11201620	002220000		1	0	1245.1044 39
11201621	002200000		1	0	388.0404 41
11201622	002180000		1	0	1245.1044 43
11201623	002160000		1	0	388.0404 45
11201624	002140000		1	0	1245.1044 47
11201625	002120000		1	0	388.0404 49
11201626	002100000		1	0	1245.1044 51
11201627	002080000		1	0	
11201628	002060000		1		1245.1044 55
11201629	002040000		1	0	388.0404 57
11201630	002020000		1	0	974.2092 59
11201631	030010000		1	0	905.4541 60
11201701	0 0.0 0.0		6		0 0 0 0 4 0 00
11201801	0.0 15.0 1				
11201901 *	0.0 15.0 1	5.0 1.8	)	1.5	0.0 0.0 1.0 60
*					

\* composition type and data format

RELAP5 Input Deck reidp3 Small Break Case 1 - Flow restrictor, non-equilibrium

*********	*******	*******
20100100		1 1 * inconel
20100101	70.0	2.3843e-03
20100102	200.0	2.5232e-03
20100103	400.0	2.8009e-03
20100104	600.0	3.0787e-03
20100105	800.0	3.3565e-03
20100106	1000.0	3.6574e-03
20100107	1200.0	3.9815e-03
20100108		4.3056e-03
20100151		
20100152		
20100153		
20100154		
20100155		
20100156		
20100157		
20100158 *	1400.0	53.7516
* control c	omponer	t cards
*		
* compute	e pressure	e difference
********	******	*****
20500100	delntn1	sum 1.45038e-4 0.0 1
20500101	• •	), p, 002040000 1.0, p, 002030000
20500200		sum 1.45038e-4 0.0 1
20500201		), p, 002080000 1.0, p, 002070000
20500300		sum 1.45038e-4 0.0 1
20500301	• •	), p, 002120000 1.0, p, 002110000
20500400		sum 1.45038e-4 0.0 1
20500401	0.0 -1.0	), p, 002160000 1.0, p, 002150000
20500500	delptp5	sum 1.45038e-4 0.0 1
20500501		), p, 002200000 1.0, p, 002190000
20500600	delptp6	sum 1.45038e-4 0.0 1
		), p, 002240000 1.0, p, 002230000
		sum 1.45038e-4 0.0 1
20500701 *	0.0 -1.0	0, p, 002280000 1.0, p, 002270000
* end of th	ne input	
*		
******	******	******

```
RELAP5 Input Deck reidp4
Small Break Case 2 - Flow restrictor, equilibrium
=SLB pressure difference across the SG tube support plats
* hot standby nonequilibrium models
100 new transnt
102 british british
105
*
******
   time step cards
*
201
     5. 1.d-7 0.005 3 2 200
                                 10000
202 5.3 1.d-7 0.00001 3 1000 20000 100000
203 6.5 1.d-7 0.000025 3 400 8000 100000
204 8.0 1.d-7 0.00005 3 200 10000 100000
205 1000.0 1.d-7 0.00010 3 100 10000 100000
    *****
   minor edit variables
*
*
301 mflowj 518000000
302 mflowj 002030000
303 mflowj 002070000
304 mflowj 002110000
305 mflowj 002150000
306 mflowj 002190000
307 mflowj 002230000
308 mflowj 002270000
309 p
          017010000
*310 p
          018010000
*311 p
           019010000
*312 p
           020010000
*313 p
          021010000
*314 p
*315 p
*316 p
          022010000
          023010000
           033010000
*317 p
           034010000
*318 p
           036010000
319 cntrlvar 1
320 cntrlvar 2
321 cntrlvar 3
322 cntrlvar 4
323 cntrlvar 5
324 cntrlvar 6
325 cntrlvar 7
```

### <u>RELAP5 Input Deck reidp4</u> Small Break Case 2 - Flow restrictor, equilib

```
Small Break Case 2 - Flow restrictor, equilibrium
*
*****
  trip input data
*
*
501 time 0 ge null 0 8.0 l
502 time 0 ge null 0 5.0 l
503 time 0 ge null 0 200.0 l
*
*
*
600 501
    ******
 hydrodynamic components
  primary side model
* hot leg and cold leg represented by tdvs
*****
1000000 inplen tmdpvol
1000101 0.0 10.0 5000.0 0.0 0.0 0.0 0.0 0.0 0
1000200 3
1000201 0.0 2235.7 547.0
1000202 5.0 2250.0 547.0
1000203 15.0 800.0 491.0
*1000204 1.0e6 800.0 491.0
*
1010000 outplen tmdpvol
1010101 0.0 10.0 5000.0 0.0 0.0 0.0 0.0 0.0 0
1010200 3
1010201 0.0 2200.0 547.0
1010202 5.0 2200.0 547.0
1010203 15.0 700.0 491.0
*
0010000 tubes pipe
0010001 60
0010101 10.956 60
0010301 1.1667 1
0010302 1.2553 3
0010303 0.5 5
0010304 1.60435 7
0010305 0.5
            9
```

0010306 1.60435 11

```
<u>RELAP5 Input Deck reidp4</u>
Small Break Case 2 - Flow restrictor, equilibrium
```

0010307 0.5 13 0010308 1.60435 15 0010309 0.5 17 0010310 1.60435 19 0010311 0.5 21 0010312 1.60435 23 0010313 0.5 25 0010314 1.60435 27 0010315 0.5 29 0010316 3.0 31 0010317 0.5 33 0010318 1.60435 35 0010319 0.5 37 0010320 1.60435 39 0010321 0.5 41 0010322 1.60435 43 0010323 0.5 45 0010324 1.60435 47 0010325 0.5 49 0010326 1.60435 51 0010327 0.5 53 0010328 1.60435 55 0010329 0.5 57 0010330 1.2553 59 0010331 1.1667 60 0010601 90.0 30 0010602 -90.0 60 0010801 0.0 0.0642 60 0011001 00000 60 0011101 000000 59 0011201 3 2250.0 547.0 0.0 0.0 0.0 60 0011300 1 0011301 9148.5 0.0 0.0 59 5000000 prminl tmdpjun 5000101 10000000 1000000 10.956 5000200 1 5000201 0.0 9148.5 0.0 0.0 5000202 1.0e6 9148.5 0.0 0.0 5010000 prmout tmdpjun 5010101 1010000 101000000 10.956 5010200 1 5010201 0.0 9148.5 0.0 0.0 5010202 1.0e6 9148.5 0.0 0.0 0020000 shell pipe 0020001 30 0020101 54.22 27

Small Break Case 2 - Flow restrictor, equilibrium

\_\_\_\_\_

RELAP5 Input Deck reidp4 Small Break Case 2 - Flow restrictor, equilibrium

-----

Sman Di	ean Gase			1030		, cyu	
0021002	00001	30					
0021101	000000	29	9				
0021201	3 1033.7	3	547.0	0.0	0.0	0.0	1
0021202	3 1033.3	4	547.0	0.0	0.0	0.0	2
0021203	3 1033.0		547.0	0.0	0.0	0.0	3
0021203	3 1032.9		547.0	0.0	0.0	0.0	4
0021205	3 1032.5		547.0	0.0	0.0	0.0	5
0021206	3 1032.0		547.0	0.0	0.0	0.0	6
0021207	3 1031.7		547.0	0.0	0.0	0.0	7
0021208	3 1031.5	6	547.0	0.0	0.0	0.0	8
0021209	3 1031.2	2	547.0	0.0	0.0	0.0	9
0021210	3 1030.7	1	547.0	0.0	0.0	0.0	10
0021211	3 1030.3	7	547.0	0.0	0.0	0.0	11
0021212	3 1030.2		547.0	0.0	0.0	0.0	12
0021213	3 1029.8		547.0	0.0	0.0	0.0	13
0021213	3 1029.3		547.0	0.0	0.0	0.0	14
		-					
0021215	3 1029.0		547.0	0.0	0.0	0.0	15
0021216	3 1028.8		547.0	0.0	0.0	0.0	16
0021217	3 1028.5		547.0	0.0	0.0	0.0	17
0021218	3 1028.0	1	547.0	0.0	0.0	0.0	18
0021219	3 1027.6	8	547.0	0.0	0.0	0.0	19
0021220	3 1027.5	2	547.0	0.0	0.0	0.0	20
0021221	3 1027.1	8	547.0	0.0	0.0	0.0	21
0021222	3 1026.6		547.0	0.0	0.0	0.0	22
0021223	3 1026.3		547.0	0.0	0.0	0.0	23
0021224	3 1026.1		547.0	0.0	0.0	0.0	24
0021225	3 1025.8		547.0			0.0	25
				0.0	0.0		
0021226	3 1025.3		547.0	0.0	0.0	0.0	26
0021227	3 1024.9		547.0	0.0	0.0	0.0	27
0021228	3 1024.8		547.0	0.0	0.0	0.0	28
0021229	3 1024.2	3	547.0	0.0	0.0	0.0	29
0021230	3 1023.1	7 :	547.0	0.0	0.0	0.0	30
0021300	1						
0021301	0.0 0	0.0	0.0	29			
	0.0625			1.0	29		
*							
*							
0350000	downc pij	2					
0350000		be					
0350101							
0350201							
0350301		3					
0350401	122.4 3						
0350601	-90.0 3						
0350801	0.00015	0.	.4275	3			
0351001	00000 3						
0351101							
0351201			547 0	0.0	0.0	0.0	1
	3 1028.6						2
0351202							
		4	J47.U	0.0	0.0	0.0	3
0351300	1	. ~	0.0	~			
0351301	0.0 0	0.0	0.0	2			

## <u>RELAP5 Input Deck reidp4</u> <u>Small Break Case 2 - Flow restrictor, equilibrium</u>

```
0300000 tubesh branch
0300001 2
           1
0300101 54.22 1.1667 0. 0. 90. 1.1667 0.00015 0.136 00100
0300200 3 1034.15 547.0
0301101 035010000 030000000 7.096 0.5 0.5 000000
0302101 030010000 002000000 4.43 5.32 5.32 000000
0301201 0.0 0.0 0.0
0302201 0.0 0.0 0.0
0340000 feedrg branch
0340001 1
            1
0340101 92.1 3.1097 0.0 0. -90. -3.1097 0.00015 0.0 00000
0340200 3 1022.48 547.0
0341101 034010000 035000000 7.096 0.0 0.0 000100
0341201 0.0 0.0 0.0
0230000 abovetb snglvol
0230101 49.43 4.9423 0.0 0.0 90. 4.9423 0.00015 0.0 00000
0230200 2 1022.72 0.03
5330000 abovetb sngljun
5330101 002010000 023000000 49.43 0.0 0.0 000100
5330110 0.0 0.0 1.0 1.0
5330201 1 0.0 0.0 0.0
0220000 speratr separatr
0220001 3 1
0220101 41.73 3.9156 0.0 0. 90. 3.9156 0.00015 0.0 00000
0220200 2 1021.14 1.0
0221101 022010000 021000000 12.828 0.84 0.47 000000
0222101 022000000 032000000 17.35 0.597 0.597 000000
0223101 023010000 022000000 41.73 8.689 8.689 000000
0221201 0.0 0.0 0.0
0222201 0.0 0.0 0.0
0223201 0.0 0.0 0.0
0320000 liqsept snglvol
0320101 17.35 0.0 86.75 0.0 0. 0.0 0.00015 0.0 00000
0320200 2 1021.26 0.92
0330000 abovf1 branch
0330001 2 1
0330101 100.7 2.9225 0.0 0.0 -90.0 -2.9225 0.00015 0.0 00000
0330200 2 1021.72 0.73
```

```
RELAP5 Input Deck reidp4
Small Break Case 2 - Flow restrictor, equilibrium
0331101 032010000 033000000 17.35 0.0 0.0 000000
0332101 033010000 034000000 79.288 0.0 0.0 000000
0331201 0.0 0.0 0.0
0332201 0.0 0.0 0.0
0530000 abovfr2 branch
0530001 2 1
0530101 100.7 3.9156 0.0 0.0 -90.0 -3.9156 0.00015 0.0 00000
0530200 2 1021.72 0.73
0531101 036010000 053000000 2.34 0.5 0.5 000000
0532101 053010000 033000000 100.7 0.0 0.0 000000
0531201 0.0 0.0 0.0
0532201 0.0 0.0 0.0
0210000 abovspr branch
0210001 2 1
0210101 152.19 2.281 0.0 0.0 90. 2.281 0.00015 0.0 00000
0210200 2 1021.12 1.0
0211101 021010000 020000000 70.75 0.0 0.0 000100
0212101 021000000 053000000 7.96 1.78 1.67 000000
0211201 0.0 0.0 0.0
0212201 0.0 0.0 0.0
0200000 spsteam snglvol
0200101 70.75 7.4502 0.0 0.0 90. 7.4502 0.00015 0.0 00000
0200200 2 1020.96 1.0
0190000 dryer separatr
0190001 3 1
0190101 171.4 0.7083 0.0 0. 0. 0. 0.00015 0.0 00000
0190200 2 1020.96 1.0
0191101 019010000 018000000 63.49 5.502 5.502 000000
0192101 01900000 036000000 2.34 0.5 0.5 000000
0193101 020010000 019000000 70.75 0.5 0.5 000000
0191201 0.0 0.0 0.0
0192201 0.0 0.0 0.0
0193201 0.0 0.0 0.0
0360000 dsdryer snglvol
0360101 2.34
              9.7312 0.0 0.0 -90. -9.7312 0.00015 0.0 00000
0360200 2
            1021.57 0.82
0180000 updryer snglvol
0180101 63.49 0.0 473.0 0.0 0. 0.0 0.00015 0.0 00000
0180200 2 1020.96 1.0
```

```
RELAP5 Input Deck reidp4
Small Break Case 2 - Flow restrictor, equilibrium
0170000 sgdoom snglvol
0170101 94.12 3.5497 0.0 0.0 90. 3.5497 0.00015 0.0 00000
0170200 2 1020.94 1.0
0380000 contrm snglvol
0380101 10000.0 200.0 0.0 0.0 90. 200.0 0.0 0.0 00000
0380200 2 14.7 1.0
5190000 abovefr sngljun
5190101 018010000 017000000 63.49 0.0 0.0 000000
5190110 0.0 0.0 1.0 1.0
5190201 1 0.0 0.0 0.0
5180000 break valve
5180101 017010000 038000000 1.388 0.0 0.0 000100
5180110 0.0 0.0 1.0 1.0
5180201 1 0.0 0.0 0.0
5180300 mtrvlv
5180301 502 503 1000.0 0.0
* heat structure input
******
11201000 60 11 2 1 0.0321
11201100 0 2
11201101 0.000438 10
11201201 1
             10
11201301 0.0 10
11201401 547.0
               11
11201501 001010000 0000 1 0 796.74 1
11201502 001020000 10000 1 0 857.24 3
11201503 001040000 10000 1 0 341.45 5
11201504 001060000 10000 1 0 1095.61 7
11201505 001080000 10000 1 0 341.45 9
11201506 001100000 10000 1 0 1095.61 11
11201507 001120000 10000 1 0 341.45 13
11201508 001140000 10000 1 0 1095.61 15
11201509 001160000 10000 1 0 341.45 17
11201510 001180000 10000 1 0 1095.61 19
11201511 001200000 10000 1 0 341.45 21
11201512 001220000 10000 1 0 1095.61 23
11201513 001240000 10000 1 0 341.45 25
11201514 001260000 10000 1 0 1095.61 27
11201515 001280000 10000 1 0 341.45 29
11201516 001300000 10000 1 0 2190.4 31
11201517 001320000 10000 1 0 341.45 33
```

Small Brea		low res	tric	:tor	<u>, equilibrium</u>
11201518	001340000	10000	1	0	1095.61 35
11201519	001360000	10000	1	0	341.45 37
11201520	001380000	10000	1	0	1095.61 39
11201521	001400000	10000	1	0	341.45 41
11201522	001420000	10000	1	0	1095.61 43
11201523	001440000	10000	1	0	341.45 45
11201524	001460000	10000	1	0	1095.61 47
11201525	001480000	10000	1	0	341.45 49
11201526	001500000	10000	1	0	1095.61 51
11201527	001520000	10000	1	0	341.45 53
11201528	001540000	10000	1	0	1095.61 55
11201529	001560000	10000	1	0	341.45 57
11201530	001580000	10000	1	0	857.24 59
11201531	001600000	0000	1	0	796.74 60
11201601	030010000	0000	1	0	905.4541 1
11201602	002010000	10000	1	0	974.2092 3
11201603	002030000	10000	1	0	388.0404 5
11201604	002050000		1	0	1245.1044 7
11201605	002070000		1	0	388.0404 9
11201606	002090000		1	0	1245.1044 11
11201607	002110000	10000	1	0	388.0404 13
11201608	002130000	10000	1	0	1245.1044 15
11201609	002150000		1	0	388.0404 17
11201610	002170000		1	0	1245.1044 19
11201611	002190000		1	0	388.0404 21
11201612	002210000		1	0	1245.1044 23
11201613	002230000	10000	1	0	388.0404 25
11201614	002250000		1	0	1245.1044 27
11201615	002270000		1	0	388.0404 29
11201616	002290000	0000	1	0	2489.277 31
11201617	002280000		1	0	388.0404 33
11201618	002260000		1	0	1245.1044 35
11201619	002240000		1	0	388.0404 37
11201620	002220000		1	0	1245.1044 39
11201621	002200000		1	0	
11201622	002180000		1	0	
11201623	002160000		1	0	
11201624	002140000		1	0	
11201625	002120000		1	0	388.0404 49
11201626	002100000		1	0	1245.1044 51
11201627	002080000		1	0	388.0404 53
11201628	002060000		1	0	
11201629	002040000		1	0	
11201630	002020000		1	0	
11201631	030010000		1		905.4541 60
11201701	0 0.0 0.0		6		0.0.0.0.4.0.00
11201801	0.0 15.0 1			1.5	0.0 0.0 1.0 60
11201901 *	0.0 15.0 1	5.0 1.5	0	1.5	0.0 0.0 1.0 60
*					

\* composition type and data format

\_\_\_\_\_

<u>RELAP5 Input Deck reidp4</u> Small Break Case 2 - Flow restrictor, equilibrium

\_\_\_\_\_

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********	******	******
20100100	tbl/fctn	1 1 * inconel
20100101	70.0	2.3843e-03
20100102	200.0	2.5232e-03
		2.8009e-03
20100104	600.0	3.0787e-03
20100105		3.3565e-03
20100106		
20100107	1200.0	3.9815e-03
20100108		4.3056e-03
20100151		
20100152		
20100153		
20100154		
20100155		
20100156		
20100157		
20100158 *	1400.0	53.7516
* control c	componer	it cards
	e pressure	e difference
* compute *		e difference
* compute *	*****	*****
* compute *	delptp1	sum 1.45038e-4 0.0 1
* compute * 20500100	delptp1 0.0 -1.0	*****
* compute * 20500100 20500101	delptp1 0.0 -1.0 delptp2	**************************************
* compute * 20500100 20500101 20500200	delptp1 0.0 -1.0 delptp2 0.0 -1.0	sum 1.45038e-4 0.0 1 ), p, 002040000 1.0, p, 002030000 sum 1.45038e-4 0.0 1
* compute * 20500100 20500101 20500200 20500201	delptp1 0.0 -1.0 delptp2 0.0 -1.0 delptp3 0.0 -1.0	sum 1.45038e-4 0.0 1 0, p, 002040000 1.0, p, 002030000 sum 1.45038e-4 0.0 1 0, p, 002080000 1.0, p, 002070000 sum 1.45038e-4 0.0 1 0, p, 002120000 1.0, p, 002110000
* compute * 20500100 20500101 20500200 20500201 20500300 20500301 20500400	delptp1 0.0 -1.0 delptp2 0.0 -1.0 delptp3 0.0 -1.0 delptp4	sum 1.45038e-4 0.0 1 0, p, 002040000 1.0, p, 002030000 sum 1.45038e-4 0.0 1 0, p, 002080000 1.0, p, 002070000 sum 1.45038e-4 0.0 1 0, p, 002120000 1.0, p, 002110000 sum 1.45038e-4 0.0 1
* compute * 20500100 20500101 20500200 20500201 20500300 20500301 20500400 20500400	delptp1 0.0 -1.0 delptp2 0.0 -1.0 delptp3 0.0 -1.0 delptp4 0.0 -1.0	sum 1.45038e-4 0.0 1 ), p, 002040000 1.0, p, 002030000 sum 1.45038e-4 0.0 1 ), p, 002080000 1.0, p, 002070000 sum 1.45038e-4 0.0 1 ), p, 002120000 1.0, p, 002110000 sum 1.45038e-4 0.0 1 ), p, 002160000 1.0, p, 002150000
* compute * 20500100 20500101 20500200 20500201 20500300 20500301 20500400 20500401 20500500	delptp1 0.0 -1.0 delptp2 0.0 -1.0 delptp3 0.0 -1.0 delptp4 0.0 -1.0 delptp5	sum 1.45038e-4 0.0 1 0, p, 002040000 1.0, p, 002030000 sum 1.45038e-4 0.0 1 0, p, 002080000 1.0, p, 002070000 sum 1.45038e-4 0.0 1 0, p, 002120000 1.0, p, 002110000 sum 1.45038e-4 0.0 1 0, p, 002160000 1.0, p, 002150000 sum 1.45038e-4 0.0 1
* compute * 20500100 20500101 20500200 20500201 20500300 20500301 20500400 20500401 20500500 20500501	delptp1 0.0 -1.0 delptp2 0.0 -1.0 delptp3 0.0 -1.0 delptp4 0.0 -1.0 delptp5 0.0 -1.0	sum 1.45038e-4 0.0 1 0, p, 002040000 1.0, p, 002030000 sum 1.45038e-4 0.0 1 0, p, 002080000 1.0, p, 002070000 sum 1.45038e-4 0.0 1 0, p, 002120000 1.0, p, 002110000 sum 1.45038e-4 0.0 1 0, p, 002160000 1.0, p, 002150000 sum 1.45038e-4 0.0 1 0, p, 002200000 1.0, p, 002190000
* compute * 20500100 20500200 20500201 20500300 20500301 20500400 20500401 20500500 20500501 20500600	delptp1 0.0 -1.0 delptp2 0.0 -1.0 delptp3 0.0 -1.0 delptp4 0.0 -1.0 delptp5 0.0 -1.0 delptp6	sum 1.45038e-4 0.0 1 0, p, 002040000 1.0, p, 002030000 sum 1.45038e-4 0.0 1 0, p, 002080000 1.0, p, 002070000 sum 1.45038e-4 0.0 1 0, p, 002120000 1.0, p, 002110000 sum 1.45038e-4 0.0 1 0, p, 002160000 1.0, p, 002150000 sum 1.45038e-4 0.0 1
* compute * 20500100 20500101 20500200 20500201 20500301 20500301 20500400 20500400 20500500 20500501 20500600 20500601	delptp1 0.0 -1.0 delptp2 0.0 -1.0 delptp3 0.0 -1.0 delptp4 0.0 -1.0 delptp5 0.0 -1.0 delptp6 0.0 -1.0	sum 1.45038e-4 0.0 1 ), p, 002040000 1.0, p, 002030000 sum 1.45038e-4 0.0 1 ), p, 002080000 1.0, p, 002070000 sum 1.45038e-4 0.0 1 ), p, 002120000 1.0, p, 002110000 sum 1.45038e-4 0.0 1 ), p, 002160000 1.0, p, 002150000 sum 1.45038e-4 0.0 1 ), p, 002200000 1.0, p, 002190000 sum 1.45038e-4 0.0 1 ), p, 002240000 1.0, p, 002230000
* compute * 20500100 20500101 20500200 20500201 20500301 20500301 20500400 20500401 20500500 20500501 20500600 20500601 20500700	delptp1 0.0 -1.0 delptp2 0.0 -1.0 delptp3 0.0 -1.0 delptp4 0.0 -1.0 delptp5 0.0 -1.0 delptp6 0.0 -1.0 delptp7	sum 1.45038e-4 0.0 1 0, p, 002040000 1.0, p, 002030000 sum 1.45038e-4 0.0 1 0, p, 002080000 1.0, p, 002070000 sum 1.45038e-4 0.0 1 0, p, 002120000 1.0, p, 002110000 sum 1.45038e-4 0.0 1 0, p, 002160000 1.0, p, 002150000 sum 1.45038e-4 0.0 1 0, p, 002200000 1.0, p, 002190000 sum 1.45038e-4 0.0 1 0, p, 002240000 1.0, p, 002230000 sum 1.45038e-4 0.0 1
* compute * 20500100 20500101 20500200 20500201 20500301 20500301 20500400 20500401 20500500 20500501 20500600 20500601 20500700	delptp1 0.0 -1.0 delptp2 0.0 -1.0 delptp3 0.0 -1.0 delptp4 0.0 -1.0 delptp5 0.0 -1.0 delptp6 0.0 -1.0 delptp7	sum 1.45038e-4 0.0 1 ), p, 002040000 1.0, p, 002030000 sum 1.45038e-4 0.0 1 ), p, 002080000 1.0, p, 002070000 sum 1.45038e-4 0.0 1 ), p, 002120000 1.0, p, 002110000 sum 1.45038e-4 0.0 1 ), p, 002160000 1.0, p, 002150000 sum 1.45038e-4 0.0 1 ), p, 002200000 1.0, p, 002190000 sum 1.45038e-4 0.0 1 ), p, 002240000 1.0, p, 002230000
* compute * 20500100 20500101 20500200 20500201 20500300 20500301 20500400 20500401 20500500 20500501 20500601 20500700 20500701	delptp1 0.0 -1.0 delptp2 0.0 -1.0 delptp3 0.0 -1.0 delptp4 0.0 -1.0 delptp5 0.0 -1.0 delptp5 0.0 -1.0 delptp7 0.0 -1.0	sum 1.45038e-4 0.0 1 0, p, 002040000 1.0, p, 002030000 sum 1.45038e-4 0.0 1 0, p, 002080000 1.0, p, 002070000 sum 1.45038e-4 0.0 1 0, p, 002120000 1.0, p, 002110000 sum 1.45038e-4 0.0 1 0, p, 002160000 1.0, p, 002150000 sum 1.45038e-4 0.0 1 0, p, 002200000 1.0, p, 002190000 sum 1.45038e-4 0.0 1 0, p, 002240000 1.0, p, 002230000 sum 1.45038e-4 0.0 1
* compute * 20500100 20500200 20500201 20500300 20500301 20500400 20500401 20500501 20500601 20500601 20500700 20500701 * * end of th *	delptp1 0.0 -1.0 delptp2 0.0 -1.0 delptp3 0.0 -1.0 delptp4 0.0 -1.0 delptp5 0.0 -1.0 delptp6 0.0 -1.0 delptp7 0.0 -1.0	sum 1.45038e-4 0.0 1 0, p, 002040000 1.0, p, 002030000 sum 1.45038e-4 0.0 1 0, p, 002080000 1.0, p, 002070000 sum 1.45038e-4 0.0 1 0, p, 002120000 1.0, p, 002110000 sum 1.45038e-4 0.0 1 0, p, 002160000 1.0, p, 002150000 sum 1.45038e-4 0.0 1 0, p, 002200000 1.0, p, 002190000 sum 1.45038e-4 0.0 1 0, p, 002240000 1.0, p, 002230000 sum 1.45038e-4 0.0 1

```
1 of 10
RELAP5 Input Deck reidp5
Large Break Case 5 - No flow restrictor, non-equilibrium, reduced water level
=SLB pressure difference across the SG tube support plats
* hot standby nonequilibrium models
100 new transnt
102 british british
105
*
******
   time step cards
*
201 5. 1.d-7 0.005 3 2 200
                                  10000
202 5.3 1.d-7 0.00001 3 1000 20000 100000
203 6.5 1.d-7 0.000025 3 400 8000 100000
204 8.0 1.d-7 0.00005 3 200 10000 100000
205 1000.0 1.d-7 0.00010 3 100 10000 100000
                  ******
*
   minor edit variables
*
*
301 mflowj 518000000
302 mflowj 002030000
303 mflowj 002070000
304 mflowj 002110000
305 mflowj 002150000
306 mflowj 002190000
307 mflowj 002230000
308 mflowj 002270000
309 p
          017010000
*310 p
          018010000
*311 p
          019010000
*312 p
           020010000
*313 p
          021010000
*314 p
          022010000
*315 p
          023010000
*316 p
           033010000
*317 p
           034010000
*318 p
           036010000
319 cntrlvar 1
320 cntrlvar 2
321 cntrlvar 3
322 cntrlvar 4
323 cntrivar 5
324 cntrlvar 6
325 cntrlvar 7
```

```
RELAP5 Input Deck reidp5
Large Break Case 5 - No flow restrictor, non-equilibrium, reduced water level
*
*****
  trip input data
*
*
501 time 0 ge null 0 8.0 l
502 time 0 ge null 0 5.0 l
503 time 0 ge null 0 200.0 I
600 501
     ******
 hydrodynamic components
    ******
  primary side model
* hot leg and cold leg represented by tdvs
***********
1000000 inplen tmdpvol
1000101 0.0 10.0 5000.0 0.0 0.0 0.0 0.0 0.0 0
1000200 3
1000201 0.0 2235.7 547.0
1000202 5.0 2250.0 547.0
1000203 15.0 800.0 491.0
*1000204 1.0e6 800.0 491.0
*
1010000 outplen tmdpvol
1010101 0.0 10.0 5000.0 0.0 0.0 0.0 0.0 0.0 0
1010200 3
1010201 0.0 2200.0 547.0
1010202 5.0 2200.0 547.0
1010203 15.0 700.0 491.0
0010000 tubes pipe
0010001 60
0010101 10.956 60
0010301 1.1667 1
0010302 1.2553 3
0010303 0.5 5
0010304 1.60435 7
0010305 0.5
            9
0010306 1.60435 11
```

0010322 1.60435 43

45

0010323 0.5

Large Break Case 5 - No flow restrictor, non-equilibrium, reduced water level
0010307 0.5 13
0010308 1.60435 15
0010309 0.5 17
0010310 1.60435 19
0010311 0.5 21
0010312 1.60435 23
0010313 0.5 25
0010314 1.60435 27
0010315 0.5 29
0010316 3.0 31
0010317 0.5 33
0010318 1.60435 35
0010319 0.5 37
0010320 1.60435 39
0010321 0.5 41

0010324 1.60435 47 0010325 0.5 49 0010326 1.60435 51 0010327 0.5 53 0010328 1.60435 55 0010329 0.5 57 0010330 1.2553 59 0010331 1.1667 60 0010601 90.0 30 0010602 -90.0 60 0010801 0.0 0.0642 60 0011001 00000 60 0011101 000000 59 0011201 3 2250.0 547.0 0.0 0.0 0.0 60 0011300 1 0011301 9148.5 0.0 0.0 59

```
5000000 prminl tmdpjun
5000101 10000000 1000000 10.956
5000200 1
5000201 0.0 9148.5 0.0 0.0
5000202 1.0e6 9148.5 0.0 0.0
*
*
5010000 prmout tmdpjun
```

5010101 1010000 101000000 10.956 5010200 1 5010201 0.0 9148.5 0.0 0.0 5010202 1.0e6 9148.5 0.0 0.0

0020000 shell pipe 0020001 30 0020101 54.22 27

Large Dr	eak case 5 - No flow re
0020102	70.0 30
0020201	54.22 2
0020202	
0020203	
	23.716 7
0020205	54.22 10
0020206	23.716 11
0020207	54.22 14
0020208	23.716 15
	54.22 18
	23.716 19
	54.22 22
	23.716 23
	54.22 26
0020214	23.716 27
0020215	70.0 29
0020301	1.2553 1
0020302	1.2553 2
0020303	0.5 4
	1.60435 6
0020305	
	1.60435 10
0020307	
	1.60435 14
0020309	
	1.60435 18
0020311	0.5 20
0020312	1.60435 22
0020313	0.5 24
	1.60435 26
0020315	
	3.2075 29
	3.4338 30
0020601	90.0 30
0020801	
0020802	
0020901	0.0 0.0 2
0020902	0.99 0.99 3
0020903	0.0 0.0 6
0020904	0.99 0.99 7
0020905	0.0 0.0 10
0020906	0.99 0.99 11
0020907	0.0 0.0 14
0020908	0.99 0.99 15
0020909	0.0 0.0 18
0020910	0.99 0.99 19
0020911	0.0 0.0 22
0020912	0.99 0.99 23
0020913	0.0 0.0 26
0020914	0.99 0.99 27
0020915	0.0 0.0 29
0021001	00100 29

Larg	ge Break	Case 5	- No flov	w restrictor,	non-eq	uilibrium	reduced	water	level

Large Dr	car dase o - no now restrictor, non	
0021002	00000 30	
0021101	000000 29	
0021201	3 1033.73 547.0 0.0 0.0 0.0	1
0021202	3 1033.34 547.0 0.0 0.0 0.0	2
0021203	3 1033.07 547.0 0.0 0.0 0.0	3
0021204	3 1032.91 547.0 0.0 0.0 0.0	4
0021205	3 1032.57 547.0 0.0 0.0 0.0	5
0021206	3 1032.06 547.0 0.0 0.0 0.0	6
0021207	3 1031.72 547.0 0.0 0.0 0.0	7
0021208		8
0021209	3 1031.22 547.0 0.0 0.0 0.0	9
0021210	3 1030.71 547.0 0.0 0.0 0.0	10
0021211	3 1030.37 547.0 0.0 0.0 0.0	11
0021212	3 1030.21 547.0 0.0 0.0 0.0	12
0021213	3 1029.87 547.0 0.0 0.0 0.0	13
0021210	3 1029.36 547.0 0.0 0.0 0.0	14
0021214	3 1029.02 547.0 0.0 0.0 0.0	15
0021215	3 1028.86 547.0 0.0 0.0 0.0	16
0021210	3 1028.53 547.0 0.0 0.0 0.0	17
0021217	3 1028.01 547.0 0.0 0.0 0.0	18
0021218	3 1027.68 547.0 0.0 0.0 0.0	19
0021219		20
0021221	3 1027.18 547.0 0.0 0.0 0.0	21
0021222	3 1026.66 547.0 0.0 0.0 0.0	22
0021223	3 1026.33 547.0 0.0 0.0 0.0	23
0021224	3 1026.17 547.0 0.0 0.0 0.0	24
0021225	3 1025.83 547.0 0.0 0.0 0.0	25
0021226	3 1025.32 547.0 0.0 0.0 0.0	26
0021227	3 1024.98 547.0 0.0 0.0 0.0	27
0021228	3 1024.82 547.0 0.0 0.0 0.0	28
0021229		29
0021230	3 1023.17 547.0 0.0 0.0 0.0	30
0021300	1	
0021301	0.0 0.0 0.0 29	
	0.0625 0.0 1.0 1.0 29	
*		
	downc pipe	
0350001		
0350101	0.0 3	
0350201		
	11.827 3	
	122.4 3	
0350601		
	0.00015 0.4275 3	
	00000 3	
	000000 2	
		1
	3 1028.64 547.0 0.0 0.0 0.0	
	3 1032.44 547.0 0.0 0.0 0.0	3
0351300		
0351301	0.0 0.0 0.0 2	

Large Break Case 5 - No flow restrictor, non-equilibrium, reduced water level

```
0300000 tubesh branch
0300001 2
            1
0300101 54.22 1.1667 0. 0. 90. 1.1667 0.00015 0.136 00100
0300200 3 1034.15 547.0
0301101 035010000 030000000 7.096 0.0 0.0 000000
0302101 030010000 002000000 4.43 5.32 5.32 000000
0301201 0.0 0.0 0.0
0302201 0.0 0.0 0.0
0340000 feedrg branch
0340001 1
            1
0340101 92.1 3.1097 0.0 0. -90. -3.1097 0.00015 0.0 00000
0340200 3 1022.48 547.0
0341101 034010000 035000000 7.096 0.0 0.0 000100
0341201 0.0 0.0 0.0
0230000 abovetb snglvol
0230101 49.43 4.9423 0.0 0.0 90. 4.9423 0.00015 0.0 00000
0230200 2 1022.72 0.39
5330000 abovetb sngljun
5330101 002010000 023000000 49.43 0.0 0.0 000100
5330110 0.0 0.0 1.0 1.0
5330201 1 0.0 0.0 0.0
0220000 speratr separatr
0220001 3
           1
0220101 41.73 3.9156 0.0 0. 90. 3.9156 0.00015 0.0 00000
0220200 2 1021.14 1.0
0221101 022010000 021000000 12.828 0.84 0.47 000000
0222101 022000000 032000000 17.35 0.597 0.597 000000
0223101 023010000 022000000 41.73 8.689 8.689 000000
0221201 0.0 0.0 0.0
0222201 0.0 0.0 0.0
0223201 0.0 0.0 0.0
0320000 ligsept snglvol
0320101 17.35 0.0 86.75 0.0 0. 0.0 0.00015 0.0 00000
0320200 2 1021.26 1.0
0330000 abovf1 branch
0330001 2 1
0330101 100.7 2.9225 0.0 0.0 -90.0 -2.9225 0.00015 0.0 00000
0330200 2 1021.72 0.93
```

```
RELAP5 Input Deck reidp5
Large Break Case 5 - No flow restrictor, non-equilibrium, reduced water level
0331101 032010000 033000000 17.35 0.0 0.0 000000
0332101 033010000 034000000 79.288 0.0 0.0 000000
0331201 0.0 0.0 0.0
0332201 0.0 0.0 0.0
0530000 abovfr2 branch
0530001 2 1
0530101 100.7 3.9156 0.0 0.0 -90.0 -3.9156 0.00015 0.0 00000
0530200 2 1021.72 0.93
0531101 036010000 053000000 2.34 0.5 0.5 000000
0532101 053010000 033000000 100.7 0.0 0.0 000000
0531201 0.0 0.0 0.0
0532201 0.0 0.0 0.0
0210000 abovspr branch
0210001 2 1
0210101 152.19 2.281 0.0 0.0 90, 2.281 0.00015 0.0 00000
0210200 2 1021.12 1.0
0211101 021010000 020000000 70.75 0.0 0.0 000100
0212101 021000000 053000000 7.96 1.78 1.67 000000
0211201 0.0 0.0 0.0
0212201 0.0 0.0 0.0
0200000 spsteam snglvol
0200101 70.75 7.4502 0.0 0.0 90. 7.4502 0.00015 0.0 00000
0200200 2 1020.96 1.0
0190000 dryer separatr
0190001 3
            1
0190101 171.4 0.7083 0.0 0. 0. 0. 0.00015 0.0 00000
0190200 2 1020.96 1.0
0191101 019010000 018000000 63.49 5.502 5.502 000000
0192101 019000000 036000000 2.34 0.5 0.5 000000
0193101 020010000 019000000 70.75 0.5 0.5 000000
0191201 0.0 0.0 0.0
0192201 0.0 0.0 0.0
0193201 0.0 0.0 0.0
0360000 dsdryer snglvol
0360101 2.34 9.7312 0.0 0.0 -90. -9.7312 0.00015 0.0 00000
0360200 2
            1021.57 1.0
0180000 updryer snglvol
0180101 63.49 0.0 473.0 0.0 0. 0.0 0.00015 0.0 00000
0180200 2 1020.96 1.0
```

Large Break Case 5 - No flow restrictor, non-equilibrium, reduced water level

```
0170000 sgdoom snglvol
0170101 94.12 3.5497 0.0 0.0 90. 3.5497 0.00015 0.0 00000
0170200 2 1020.94 1.0
0380000 contrm snglvol
0380101 10000.0 200.0 0.0 0.0 90. 200.0 0.0 0.0 00000
0380200 2 14.7 1.0
5190000 abovefr sngljun
5190101 018010000 017000000 63.49 0.0 0.0 000000
5190110 0.0 0.0 1.0 1.0
5190201 1 0.0 0.0 0.0
5180000 break valve
5180101 017010000 038000000 4.6 0.0 0.0 000100
5180110 0.0 0.0 1.0 1.0
5180201 1 0.0 0.0 0.0
5180300 mtrvlv
5180301 502 503 1000.0 0.0
* heat structure input
*****
11201000 60 11 2 1 0.0321
11201100 0 2
11201101 0.000438
                  10
11201201 1
             10
11201301 0.0 10
11201401 547.0
                11
11201501 001010000 0000 1 0 796.74 1
11201502 001020000 10000 1 0 857.24 3
11201503 001040000 10000 1 0 341.45 5
11201504 001060000 10000 1 0 1095.61 7
11201505 001080000 10000 1 0 341.45 9
11201506 001100000 10000 1 0 1095.61 11
11201507 001120000 10000 1 0 341.45 13
11201508 001140000 10000 1 0 1095.61 15
11201509 001160000 10000 1 0 341.45 17
11201510 001180000 10000 1 0 1095.61 19
11201511 001200000 10000 1 0 341.45 21
11201512 001220000 10000 1 0 1095.61 23
11201513 001240000 10000 1 0 341.45 25
11201514 001260000 10000 1 0 1095.61 27
11201515 001280000 10000 1 0 341.45 29
11201516 001300000 10000 1 0 2190.4 31
11201517 001320000 10000 1 0 341.45 33
```

## **RELAP5 Input Deck reidp5**

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Large Break Case 5 - No flow restrictor,	non-equilibrium. reduced water leve!

Large Died	in dast o - in		531	nou	, non-equilibrium, i
11201518	001340000	10000	1	0	1095.61 35
11201519	001360000	10000	1	0	341.45 37
11201520	001380000	10000	1	0	1095.61 39
11201521	001400000	10000	1	0	341.45 41
11201522	001420000	10000	1	0	1095.61 43
11201523	001440000	10000	1	0	341.45 45
11201524	001460000	10000	1	0	1095.61 47
11201525	001480000	10000	1	0	341.45 49
11201526	001500000	10000	1	0	1095.61 51
11201527	001520000	10000	1	0	341.45 53
11201528	001540000	10000	1	0	1095.61 55
11201529	001560000	10000	1	0	341.45 57
11201530	001580000	10000	1	õ	857.24 59
11201531	001600000	0000	1	õ	796.74 60
11201601	030010000	0000	1	ŏ	905.4541 1
11201602	002010000	10000	1	0	974.2092 3
11201603	002030000	10000	1	õ	388.0404 5
11201603	002050000	10000	1	0	1245.1044 7
11201605	002070000	10000	1	0	388.0404 9
11201606	002090000	10000	1	0	1245.1044 11
11201607	002110000	10000	1	0	388.0404 13
11201608	002130000	10000	1	0	1245.1044 15
11201609	002150000	10000	1	0	388.0404 17
11201610	002170000	10000	1	0	1245.1044 19
11201611	002190000	10000	1	0	388.0404 21
11201612	002210000	10000	1	0	1245.1044 23
11201613	002230000	10000	1	0	388.0404 25
11201614	002250000	10000	1	0	1245.1044 27
11201615	002270000	10000	1	0	388.0404 29
11201616	002290000	0000	1	0	2489.277 31
11201617	002280000		1	0	388.0404 33
11201618	002260000	-10000	1	0	1245.1044 35
11201619	002240000	-10000	1	0	388.0404 37
11201620	002220000	-10000	1	0	1245.1044 39
11201621	002200000	-10000	1	0	388.0404 41
11201622	002180000	-10000	1	0	1245.1044 43
11201623	002160000	-10000	1	0	388.0404 45
11201624	002140000	-10000	1	0	1245.1044 47
11201625	002120000	-10000	1	0	388.0404 49
11201626	002100000	-10000	1	0	1245.1044 51
11201627	002080000		1	0	388.0404 53
11201628	002060000		1		1245.1044 55
11201629	002040000		1	Ō	
11201630	002020000			ŏ	
11201631	030010000				905.4541 60
11201001	0 0.0 0.0		6		
11201801	0.0 15.0 1			1.5	0.0 0.0 1.0 60
11201901	0.0 15.0 1			1.5	0.0 0.0 1.0 60
*	0.0 IJ.0 I	0.0 1.0	,	1.0	
*					

\* composition type and data format

\*

<u>RELAP5 Input Deck reidp5</u> Large Break Case 5 - No flow restrictor, non-equilibrium, reduced water level

Large Brea	<u>ak Case (</u>	5 - No flow restrictor, non-equilibrium,
********	********	******
20100100	tbl/fctn	1 1 * inconel
		2.3843e-03
20100102	200.0	2.5232e-03
20100103	400.0	2.8009e-03
20100104	600.0	3.0787e-03
20100105		
		3.6574e-03
		3.9815e-03
		4.3056e-03
20100151		
20100152		
20100153		
20100154	600.0	54.9895
20100155	800.0	54.7069
20100156	1000.0	54.3982
20100157	1200.0	54.0907
20100158	1400.0	53.7516
*		
	componer	nt cards
*		
* compute	e pressure	e difference
****	ول	*****
20500100		sum 1.45038e-4 0.0 1
20500101		0, p, 002040000 1.0, p, 002030000
20500200		sum 1.45038e-4 0.0 1
20500201		0, p, 002080000 1.0, p, 002070000
20500300 20500301		sum 1.45038e-4 0.0 1
		0, p, 002120000 1.0, p, 002110000 sum 1.45038e-4 0.0 1
20500400	•••	0, p, 002160000 1.0, p, 002150000
20500401		
20500500		sum 1.45038e-4 0.0 1 D, p, 002200000 1.0, p, 002190000
20500600		sum 1.45038e-4 0.0 1
20500600		D, p, 002240000 1.0, p, 002230000
		sum 1.45038e-4 0.0 1
		D, p, 002280000 1.0, p, 002270000
*	0.0 -1.0	, p, 002200000 1.0, p, 002210000
* end of th	ne input	
*		

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