



International Agreement Report

Assessment of RELAP5/MOD2, Cycle 36.04 Against FIX-II Guillotine Break Experiment No. 5061

Prepared by
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Swedish Nuclear Power Inspectorate
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Office of Nuclear Regulatory Research
U.S. Nuclear Regulatory Commission
Washington, DC 20555

July 1989

Prepared as part of
The Agreement on Research Participation and Technical Exchange
under the International Thermal-Hydraulic Code Assessment
and Application Program (ICAP)

Published by
U.S. Nuclear Regulatory Commission

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National Technical Information Service
Springfield, VA 22161



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STUDSVIK ENERGITEKNIK AB

STUDSVIK/NP-86/109

1986-10-28

SKI Project 85026, 13.3-917/84

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ICAP

Assessment of RELAP5/MOD2, Cycle 36.04 Against
FIX-II Guillotine Break Experiment No 5061

ABSTRACT

The FIX-II guillotine break experiment No. 5061 has been analyzed using the RELAP5/Mod2 code. The code version used, Cycle 36.04, is a frozen version of the code.

Four different calculations were carried out to study the sensitivity of initial coolant mass, junction options and break discharge line nodalization. The differences between the calculations and the experiment have been quantified over intervals in real time for a number of variables available from the measurements during the experiment.

The break mass flows were generally underpredicted at the same time as the depressurization rate was overpredicted.

Approved by

27 May 14

Kjell Johansson



LIST OF CONTENTS

	<u>Page</u>
1. INTRODUCTION	3
2. FACILITY AND TEST DESCRIPTION	5
2.1 Test facility	5
2.2 The experiment	7
2.3 Measurement uncertainty	9
3. CODE AND MODEL DESCRIPTION	10
3.1 The code features	10
3.2 The Input Model	11
4. THE BASE CASE CALCULATION	14
5. SENSITIVITY RESULTS AND DISCUSSION	18
5.1 Case B	18
5.2 Case C	20
5.3 Case D	21
5.4 Discussions	21
6. RUN STATISTICS	23
7. CONCLUSIONS	24
REFERENCES	26
FIGURES	28
TABLES	35
APPENDICES	
A. Input listings	
B. Data comparison plots	
C. Calculation of data uncertainties	
D. Description of the accompanying data package	



1. INTRODUCTION

An International Thermal-Hydraulic Code Assessment and Applications Program (ICAP) is during the present years being conducted by several countries under the coordination of the USNRC (1). The goal of the program is to make quantitative statements regarding the prediction capabilities of current best-estimate thermal-hydraulic computer codes. Such codes have been used for many years as state-of-the-art instruments to study and verify numerical and correlative computation models against results obtained in experiment. Some of those codes have reached a high degree of sophistication and do comprise models for mainly all processes which are essential to thermal-hydraulic scenarios in nuclear reactor application. So far, however, those codes did not achieve the status as reactor licensing tools, such as fulfilling the Appendix K rules (2), although they are often applied for other calculations. The present ICAP aims to quantify uncertainties of the codes to allow their use for licensing purposes.

Sweden's contributions to ICAP encompass assessment calculations using the two thermal-hydraulic codes TRAC-PWR (3) and RELAP5/MOD2 (4). The assessment calculations are conducted by Studsvik Energiteknik AB sponsored by the Swedish Nuclear Power Inspectorate.

The calculation presented in this report concerns a FIX-II experiment for a 200 % double-ended guillotine break. This experiment, Test No. 5061, was conducted during the second experimental period. Table 1 gives a short information about experiments done during that period.

A description of the test facility and this particular test is provided in Chapter 2. A description of the input model is given in Chapter 3. The base case and sensitivity calculations are discussed in Chapters 4 and 5. Run statistics are given in Chapter 6. General conclusions are drawn in Chapter 7.

Appendix A contains the complete input lists. The data comparison plots are included in Appendix B. Results of the statistical analyses of differences between experiment and predictions for discrete time intervals are included in Appendix C. Finally, Appendix D describes the data package on magnetic tape prepared for use on the ICAP evaluation work.

2. FACILITY AND TEST DESCRIPTION

The FIX-II integral test facility was completed at the end of 1981. It has been run by Studsvik Energiteknik AB under contract to the Swedish Nuclear Power Inspectorate. The experimental program comprises investigations of the fuel-to-coolant heat transfer. Various blowdown and pump trip situations conceivable in Swedish BWR's are simulated.

2.1 Test facility

The test facility itself is shown in Figure 1. The volume scaling is 1:777 of the Oskarshamn-II reactor, which is of the ASEA-ATOM external recirculation pump design. An exhaustive description of the FIX-II test facility may be obtained from Ref (5), which also provides additional references where various problems pertaining to the construction period are discussed. Therefore, only some fundamental aspects of the facility will be presented here.

The core model involves a full length rod bundle, which in the geometry is closely related to a fuel element of the ASEA-ATOM design and electrically heated by DC. Here, however, there are only 6 x 6 rod simulators instead of the 8 x 8 rods in a fuel element. Figures 2 and 3a show details from the core simulator design. As seen, filler bodies are placed between the square-section fuel channel and the circular-section pressure vessel to reduce the water-filled volume, which otherwise may influence the test by the leakage of steam to the upper plenum. The water surrounding the fillers is externally recirculated and cooled by 200 to 250 kW.

The upper part of the pressure vessel, Figure 3b, holds the steam separator and the steam condenser volume with its three sprinklers. During steady state power operation the steam outlet is closed. The turbine power is modelled by the partial circulation of water from the downcomer through an external 6 MW cooler with feedback to the sprinklers of the steam condenser and into the upper part of the downcomer. The flow rate in the two branches with cooled water is adjusted to control the pressure and the inlet subcooling. The remaining downcomer flow, representing the recirculation coolant flow in the reference reactor, splits at the lower downcomer end into two loops. One loop represents three of the intact recirculation lines of the reference reactor, while the other loop, representing a fourth recirculation line, incorporates the break devices. Both loops have a recirculation pump. The intact loop pump speed is regulated according to a pre-determined speed history.

The FIX-II has, as part of the core model, an external bypass simulator through which about 12 % of the recirculation mass flow is diverted through a control valve. This bypass is heated separately to represent the channel wall heat transfer. At the lower end of the bypass, Figure 3c, there is a stagnant water volume to simulate the reference reactor space for the control rod guide tubes.

Since the FIX-II facility has been designed for blowdown experiments only, no emergency core cooling equipment is installed.

The data collection system is constructed around a signal processor controlling 192 measurement channels. The selection of measurements is made in a signal exchange terminal. A multipurpose minicomputer transfers the raw-data of measured parameters to a magnetic tape. From this tape, the final analysis at the central computer gives the desired tables and plots from an experiment. The data acquisition system includes measurements to obtain:

- pressures (PT)
- differential pressures (dPT)
- temperatures of fluids (TE)
- mass flows (dPT, PT, TE)
- electric currents (I) and voltages (U)
- pump speeds (nT)
- water level positions (CE)
- valve positions

at places shown in the instrumentation diagram, Figure 4.

For recording clad temperatures there were about 100 thermocouples engaged at 16 axial levels of the heated length in the 36-rod bundle.

2.2 The experiment

The preparation of the experiment is initiated several hours before the actual blowdown. For the heat-up of the facility, a 200 kW preheater is involved for a period lasting about 5 h. The recirculation pumps are running during this period too. Initial conditions are then established by switching the power supplies to the bundle and

to the bypass with the 6 MW cooler and the condenser spray in operation. The preheater is now disconnected. For about 10 to 30 minutes, the electric power to the rod bundle and the bypass heating is gradually increased until the initial test conditions are reached. Necessary calibrations are made, and once the equilibrium conditions are finally approved, the sequency control equipment is activated for break opening, valve manoeuvres, power reduction, pump speed changes and so forth, according to a programmed scheme for the test. For the guillontine break test No. 5061, the transient ends 27.3 s after opening of the break.

In the present FIX-II experiment, the speed of the pump in the intact recirculation line decreased from the break time to about 20 % of the initial speed at end of the transient. The speed of the broken recirculation line pump was not explicitly controlled.

The break flow escaping through the fast opening break valves, Figure 1, are discharged into the receiving tanks, T2 and T3. Initially, the tanks are partly filled with cold water for efficient pool condensation of the break flows.

The guillotine break assembly consists of one connection to the line from pump P2 and one connection to the lower plenum. Break flow limiting orifices, downstream of the break isolation valves, consist of an exchangeable conical inlet part followed by a restriction pipe. In experiment No. 5061, each restriction pipe and flange diameter were 21.6 mm corresponding to a 100 % area of one recirculation line. The total break area for both connections is thus 200%.

Apart from the heat removal from the filler body space, see Chapter 2.1, some 100 kW are also lost by the non-perfect insulation encapsulating the recirculation lines and the pressure vessel. The magnitude of the steady state heat losses was one argument for not performing experiments with very small break areas at FIX-II.

The main measured parameters for the steady state before break are reproduced from Ref (6) in Table 4. The test performance chronology, related to the programming of the sequence control equipment, is given in Table 5.

Experimental raw data were collected for the whole period of the transient. However, internal flows were then only evaluated until about 7 s due to uncertainties in the two-phase flow rate measurements.

A summary of the main results (including event times, maximum cladding temperatures and some peak mass flows) is given in Table 6.

2.3 Measurement uncertainty

To obtain estimates for the accuracy of the measured data, test procedures were adapted within the experimental program. Probable errors and errors corresponding to a 95 % confidence level as derived from these tests are summarized in Table 2a. The probable errors of derived quantities, mostly mass flows, are given in Table 2b. The pump speeds are measured using a tachometer of a 1 r/s accuracy. The pump characteristics were verified against the manufacturer's data for cold water single phase operation.

3. CODE AND MODEL DESCRIPTIONS

The assessment calculation for the FIX-II experiment No. 5061 was done using the RELAP5/Mod2, Cycle 36.04 code received at the beginning of February 1985. The code was implemented in June 1986 on a CDC 170-810 computer. The descriptive document available for this code at the time of preparing the calculation input was the rather detailed code manual (4) also explicitly containing an input data requirements manual. The code features are discussed in Chapter 3.1.

The calculation model is closely related to the two previous ICAP calculations for the FIX-II experiments No. 3027 Ref (7) and No. 3051 Ref (8). The main differences in the input concern the double-ended break geometry. Details of the input are discussed in Chapter 3.2.

3.1 The Code Features

An extensive code description for the RELAP5/Mod2 is given in the Ref 4. The main characteristics of the code are summarized in Table 3.

Since the RELAP5/Mod2 code is primarily developed for PWR application, the question arises whether some important features are missing in the code for a BWR-type application like the present FIX-II experiment. One such feature could be deficient modeling of droplet flow in RELAP5/MOD2 for reflood and core top spray. The FIX-II facility does not have a core top spray cooling as the facility is designed for experiments until end of blowdown only. The steady state cooling, however, is accomplished by a cold water injection.

at the top of an internal condenser space above the core and the steam separator. The condenser space is voluminous; and it is assumed that the condenser spray partly vaporizes while the rest, reaching saturation, has no impact on the core behaviour. Modelling of droplet flows is therefore in actuality not addressed in this study.

3.2 The Input Model

The model geometry used in the present calculations is closely related to geometries used in several previous calculations for FIX-II experiments using previous RELAP5/Mod1 code versions (7 and 8). The nodalization diagram for the geometric modelling used is shown in Figure 5. Figures 6 and 7 depict the modelling of the geometry of the test facility.

To reproduce fundamental measured steady state quantities, see Table 4, the input for the steady state runs was modified by some additional components and control systems:

- I To obtain the steady state dome pressure, a time dependent volume outside the opened steam relief valve was added. This volume had the experimentally measured dome pressure.
- II The speed of the pumps P1 and P2 were controlled using the RELAP5 control system to reproduce the measured mass flows.
- III To divert the correct mass flow into the core bypass, the junction from the lower plenum was modelled as a motor valve. By trip logic, the opening of that valve was controlled to give the experimental bypass mass flow. When entering into the transient calculation, the valve setting was fixed.

- IV The measured steam separator collapsed level was satisfied by connecting an auxiliary time dependent volume to the top of the steam separator. The connecting junction was modelled to adjust the collapsed level by water addition depending on the level offset.
- V To eliminate the mass flow of the pressurizer discussed under item I the common temperature of the condenser spray water and the feedwater was adjusted within a span of 2K from the measured temperature. The level control flow, item IV, then also became negligible.

For the condenser spray water and the feedwater temperature control (item V) had not been applied for any previous FIX-II calculation. For the present experiment this was necessary because of an inconsistency in the heat balance in the measured initial conditions, Table 4. The temperature of the coolants, had to be increased by 1.8 K to match the heat balance. This is, within the measurement error limits for fluid temperatures, Table 2a.

Another difference from the previous FIX-II calculations is the lower fluid temperature in the two break flow lines Plot B.34. The experimental temperature on the plot obtained at the T-piece measures the recirculated water temperature under steady state. The first calculations indicated too low break flows during the first one or two seconds. By the lower fluid temperature in the discharge lines, the initial break discharge was better predicted. For temperature stability in the initial steady state the boundary heat structures of the discharge pipes were assumed to have insulated outer boundary conditions.

The input of the steady state was in the present calculation made as complete as possible to also cover the transient actions. The steady state controls were disconnected by a first trip and the remaining trips followed to simulate the system actions. In the transient restart the first trip is set at zero time with a new initiation of the time scale. Until the second trip, which is the one initiating the physical transient, the transient calculation is run at the initial state as test for stability. The sensitivity calculations also start with steady state calculations from inputs having complete sensitivity updates.

The discharge flow from the downcomer side break did in the first test calculations give rise to some doubt about the pump P2 head curve dependence of the volume flow (9). From the initial single-phase discharge flows of some split break FIX-II experiments (Nos 3025, 3027, 3031, 3051 and 3061 at lower flow rates) the accuracy of the most important parts of the single-phase head curves were confirmed.

4. THE BASE CASE CALCULATION

The transient calculation of the base case (called Case A) was based on the restart file obtained from the steady state calculation. To verify the quality of the steady state, the opening of the break was delayed by 5 s.

The calculation of the transient was carried out without any particular problems. The smooth lapse of the CPU-time, Plot B.37 and of the computation mass error, Plot B.39, indicate that.

A set of results from the base case calculation and the sensitivity calculations were selected to fulfil the requirement on assessment parameters given in Table 3 of Ref 1. Those parameters are listed in Table 8 and the comparison plots are reproduced in Appendix B. Since some of the parameters are not available from the experimental data, only comparisons between different calculations are shown in some of the plots. For the internal mass flow comparisons, it should be emphasized that the experimental data are not reliable after voiding has begun which for most measurements occurs about 7 s after the break opening.

The spray flow and the feedwater valves, were closed immediately after the break, see Table 5. The break signal also initiates closure of the valve in the broken recirculation line (V103). There is a good agreement between calculation and experiment of the mass flow rate through the steam relief valve, plot B.28. However, the break mass flows which in the experiment are measured by the increasing content of flow receiving tanks, plots B.32 and B.33, have obviously been underestimated in the base case calculation.

A problem with the determination of break flow should be noted. The discharge flows enter two collection tanks filled with a large amount of cold water. The discharged mass is evaluated using the pressure difference from the bottom to the water level in the tanks. The discharge pipes also include perforated tubes inside the collecting tanks. The volumes of these pipes amount about $.037 \text{ m}^3$ for the downcomer side and about $.042 \text{ m}^3$ for the vessel side tubes. These volumes are probably steam-filled and small steam jets may even occur outside of the perforated parts during the blowdown. The actual level fall back at end of the transient when the break valves close, is less than the volumes of the perforated tubes. Consequently, at the end of the transient same water was present in each of the discharge pipes.

It can be concluded that the bias in the break mass loss must have varied during the transient. However, the initial bias, was apparently nearly the same as the bias near the end of the test. The mass flow rates which are obtained from the differentiated mass inventory history may contain large errors in instantaneous values.

The calculated system pressure, Plots B.21, B.22 and B.36, is in the base case decreasing too rapidly. The depressurization rate responds on the break mass flow and quality, on the continued system heating and on the initial fluid mass as the main quantities. The entalpy increase comes partly from the core and partly from the by-pass heating. The filler body space cooling is also rather well defined during the transient because of the known initial cooling capability. Least

well known is the heat from passive structures. Plot B.3 shows that this heating is considerable and is even larger than the decay heat after 13 s. The heat structure modelling has been developed based on previous FIX-II calculations for smaller break areas. From the results of these calculations the heat structure modelling can be assumed to be adequate. Therefore, errors in the initial system mass content is suspected to be responsible for the underpredicted system pressure. The first sensitivity calculation is devoted to this question.

The predicted core inlet temperature, Plot B.11, and the core outlet temperature are close to saturation temperatures. The same applies for other system fluid temperatures, Plots B.19, B.20 and B.34. The core inlet temperatures show, Plot B.11, larger initial subcooling in the experiment than is predicted. A minor part of the discrepancy is a consequence of the slight overtemperature of the feedwater necessary to maintain the initial heat balance, see Chapter 3.2. As the core inlet mass flow reverses immediately after break, Plot B.2, a faster core inlet temperature rise in the experiment had been expected than Plot B.11 shows.

Plots B.1, B.14 and B.29 show calculated fluid densities at the core bottom, at the reactor vessel bottom and upstream of the break. Fluid densities were not directly measured in the experiment.

The fluid inventories of the core, Plot B.13, the upper plenum, Plot B.17, the downcomer, Plot B.15, and of the lower plenum, Plot B.16, are compared as differential pressures which are directly measured in the experiment.

Notable is the discrepancy in the lower plenum pressure difference in the time interval up to 5 s, Plot B.16. This, together with the discrepancy in the differential pressure over the core inlet restriction, Plot B.2, verifies that the vessel inlet mass flow, Plot B.26, is larger than predicted for this time interval. The mass flow escaping from the lower plenum towards the break appears in the experiment not to be completely consistent with the break flow (compare with Plot B.33).

The comparisons of the rod clad temperatures are done at the clad inner surface which is closest to the thermocouple positions of the electrically heated rods in the experiment. Above the core midplane, levels 7, 9, 12 and 15, the dryouts are predicted to occur later than in the experiment. Actually, the calculated dryout of all levels was delayed until the void was .985 or higher. In RELAP5/Mod2 the critical heat flux is calculated according to a correlation using $1-\alpha$ (α is the steam void) as a factor. This should be compared with the corresponding RELAP5/Mod1 correlation using $.96-\alpha$ as a factor in the critical heat flux expression. The latter gave better agreement with FIX-data. The delay in the calculated dryouts is probably a result of the critical heat flux correlation rather than of core voids.

5 SENSITIVITY RESULTS AND DISCUSSIONS

By variation of the calculation model from the base case, Case A, three additional calculations were carried out. These sensitivity calculations are characterized by the following changes:

Case B Increased initial liquid mass

Case C As Case B and changes in the pumps outlet restriction modelling

Case D As Case B and a denser nodalization on the downcomer side main break flow path

5.1 Case B

The base case calculation failed to predict several parameters reasonably well. The depressurization did proceed too fast while the fluid mass discharged through the breaks was underpredicted. The reason could be an underestimate of the initial fluid mass which corresponded to the measured downcomer collapsed liquid level. The same problem had previously been recognized for the FIX-II split break No. 3027, Ref (7).

The underestimate of the initial mass is mainly a consequence of the calculated droplet content in the spray condenser. The condenser constitutes about three quarters of the total system volume.

The water droplets entering the condenser before experiment are formed by injection nozzles giving droplet diameters smaller than assumed by the code which uses a fixed Weber-number for the annular mist flow regime. For the FIX-II experiment No. 3027 an underestimate of the condenser water mass by 26 kg had followed from an estimated difference in the droplet falling velocity Ref (7).

The total loss of mass through the two guillotine breaks and the steam relief valve was estimated to have been 298 kg in the experiment Ref (6). The remaining mass in the system after test end is not accurately known. The lower plenum volume, however, contains no water after test termination. No water could be identified elsewhere in the system. Thus, assuming saturated steam in the system implies additionally 12.5 kg which added to the total transient mass discharge gives an initial system mass of 310 kg.

In the split break calculation for the FIX-II experiment No. 3027 water had been added by assuming a higher initial water level in the downcomer than measured in the experiment. For the present calculation it was assumed that the higher water content in the condenser was a consequence of a lower droplet velocity in the experiment as compared to the water velocity predicted by the code. This means that the water transit time through the condenser volumes should be extended. Therefore the lengths of the condenser volumes 11 and 12, see Figure 5, were increased by a common factor while retaining their volumes. A length factor of 4.8 gave an initial mass of about 314 kg. The factor 4.8 was just a little less than that factor by which the code would start water accumulation in the condenser.

The results from the Case B calculation did generally compare better with the experiment than the base case results. The depressurization, Plot B.22, was fairly well predicted. The vessel side break flow, Plot B.33, turned out quite well while the downcomer side break flow, Plot B.32, still was underestimated.

5.2 Case C

The break discharge from the vessel side compared well in the Case B with the experiment, Plot B.33, while that from the downcomer side, Plot B.32, still was underestimated. There were no obvious reasons to introduce additional discharge coefficients since piping geometries close to the two break regions were very similar.

From the downcomer to the break the fluid passes the pump P2 outlet restriction. A pressure loss of more than .5 MPa is caused by the restrictions during the transient. An increased flashing in the pipes downstream of the restriction could produce different discharge conditions compared to the vessel side break opening.

The outlet restriction at the pump P2 has a diameter of 22 mm which is nearly the same as the diameter of the break opening. The junction options used at the previous two calculations had been choked flow, smooth area change and unequal phase velocities. In addition a flow loss coefficient also used in some previous applications had been utilized. With this modelling of the flow restriction the pressure drop had been slightly overpredicted during the first part of the transient in previous calculations.

The pressure loss of the pump P2 outlet restrictions had been measured at various flow conditions during the running-in experiment Ref (9). A best fit loss coefficient was determined as:

$$\zeta = 347 \times \text{Re}^{-.056}$$

Assuming a water flow of 12 kg/s to be representative for the first part of the transient a loss coefficient of 165 was calculated. A test calculation showed that assuming abrupt area change with choked flow, and no explicit extra loss coefficient, gave just that loss coefficient. For the Case C calculations these junction options, also assuming homogeneous two phase flow and the restriction areas as in the experiment, were used at the outlet restrictions of both recirculation pumps.

5.3 Case D

The Case D sensitivity calculation addresses the nodalization density. The steam separator (vol 21), the downcomer (vol 71), and broken line (vols 95 and 96) volumes were on the downcomer side further divided to give about the double amount of nodes. These model changes were done to the Case B input data deck.

5.4 Discussion

The experimental rod temperatures in the plots B.4 through B.10 are mean values of all available temperature measurements at the individual core levels. The absolute maxima of the rod temperatures measured at each level are indicated on the plots. The individual temperature maxima at a level do distribute over ranges of even more than 100 K. Plots of the individual rod temperature measured in the experiment are found in Ref (6).

In view of the temperature distribution in the experiment the predictions obtained from the calculations Cases A, B and C are acceptable at the high peak temperature levels. At the lowest core level, Plot B.4, all the predictions failed with the exception of the very early temperature rise. Actually, one rod close to the box shows a similar level 1 temperature behaviour as the predictions. The reason for the disagreement to the other rod temperatures at the lowest core level may be due to three-dimensional flow effects or to the erroneously early core inlet flow reversal.

The quite different core temperature predictions in the Case D calculation, using a denser nodalization in the downcomer side discharge path, is remarkable. The depressurization rate of that calculation was most badly predicted during the later half of the transient but rather good during the times of high clad temperatures. No core data like the fluid density at the bottom, Plot B.1, the boundary fluid temperatures, Plots B.11 and B.12, or the core pressure difference, Plot B.13, are in the Case D results significantly different from the previous calculation cases. Typical of the Case D calculations are lower break flow fluid densities, compare Plots B.14 and B.29, causing a larger amount of remaining water in the core although the break flow was similar to that of the previous calculations.

6. RUN STATISTICS

The transient calculation model used with the base case RELAP5/Mod2 prediction for the FIX-II test No. 5061 was modelled by:

60 volumes
62 junctions
70 heat structures

The volumes number includes two pump components and six time dependent volumes and among the junctions there are three valve components and four time dependent junctions.

The computer efficiency is summarized in Table 7 from the Major Edit printouts, see also Plot B.37. The table also gives the number of time step reductions from requested time steps forced by the code internal stability control.

The transient calculation needs were:

computer time	CPU = 1 289 s
number of time steps	DT = 726
number of volumes	C = 60
transient real time	RT = 28 s

from which also a code efficiency factor (3) of

$$\text{CPU} \times 103 = 29.6 \text{ C} \times \text{DT}$$

is obtained. The computer used was a Cyber 170-810.

7 CONCLUSIONS

A double ended quillotine break in the FIX-II facility was assessed in the present calculations using the RELAP5/Mod2 code. Four calculations were carried out; one base case and three sensitivity calculations with variations in initial mass content and nodalization.

In the steady state a small inconsistency with the heat balance appeared using the initial conditions from the experiment. Using previously evaluated data for the heat losses, a 1.8 K hotter feedwater temperature had to be assumed. This is within the experimental uncertainty.

Concerns about the system total mass and pressure behaviour arose in all the calculations. For the base case the measured initial water level was used. The calculated system pressure decreased significantly faster than in the experiment. The reason was that the base case calculation had a too low initial fluid mass. By using more elongated spray condenser volume a realistic droplet velocity could be simulated. This increased the mass content by about 16 kg. The true initial mass of the experiment is uncertain.

The two last sensitivity calculations were conducted to achieve better agreement in the discharge mass flow and distribution of the flow contributions from the two sides. None of these calculations actually gave a better prediction than Case B. Particularly the reduction in prediction quality of the calculations using smaller control volumes along one discharge flow path (Case D) was unexpected.

As for previous FIX-II calculations the predicted dryout was delayed at the higher core levels as a consequence of the void dependence of the RELAP5/Mod2 dryout correlation.

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STUDSVIK/NR-84/363.

1986-10-28

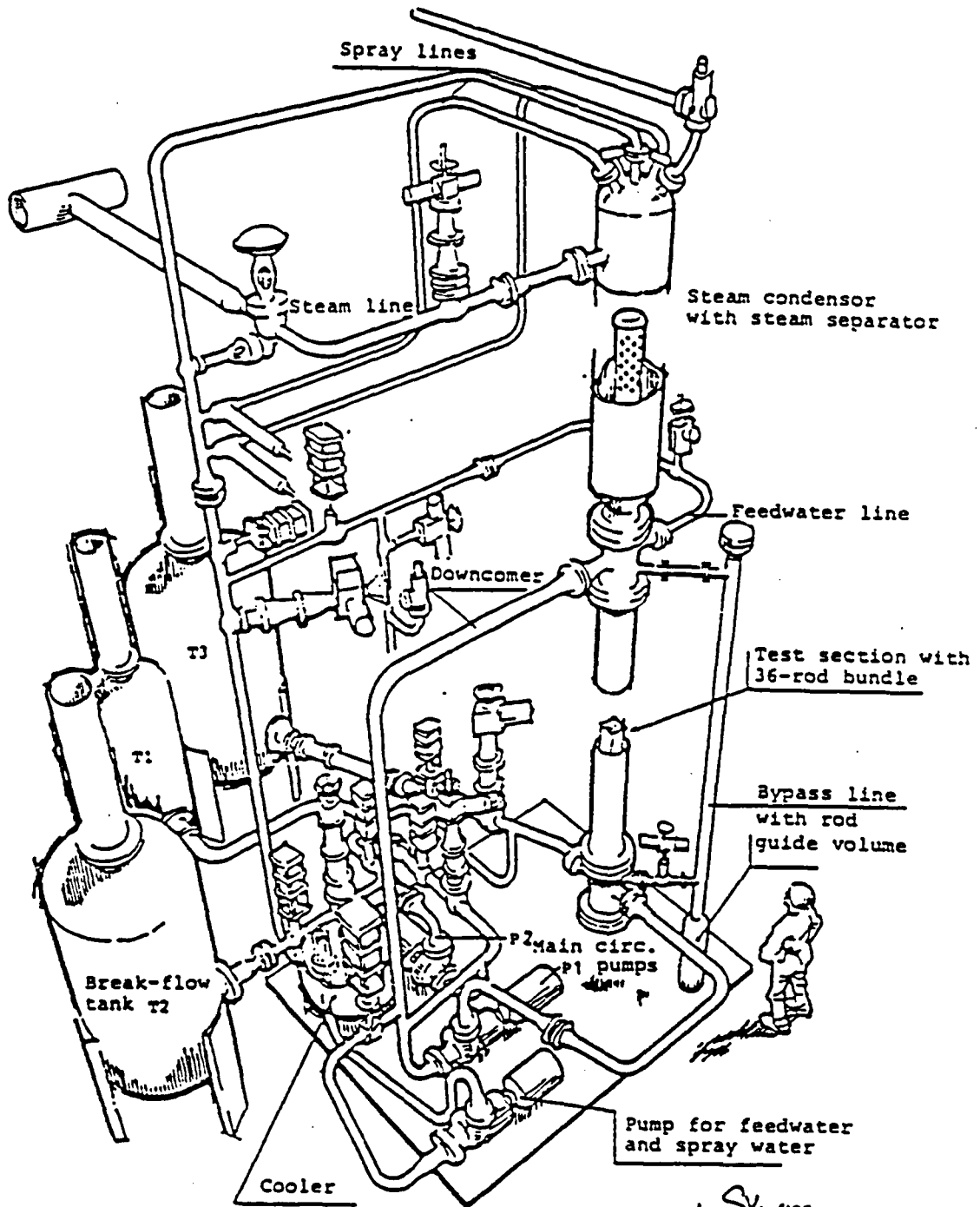


Figure 1

General view of the FIX-II facility.

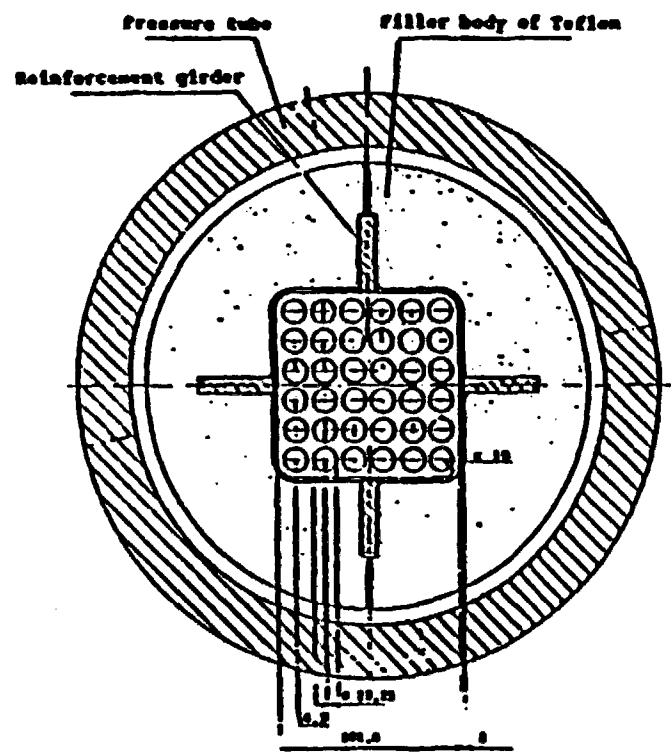


Figure 2.a
Cross section of pressure vessel and rod bundle.

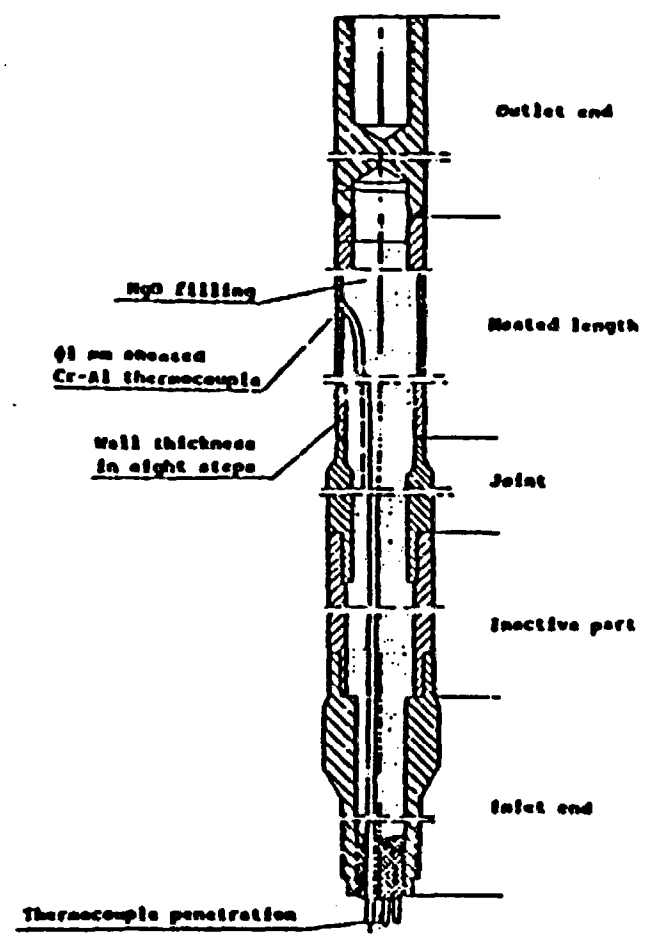


Figure 2.b
Design of a fuel rod simulator.

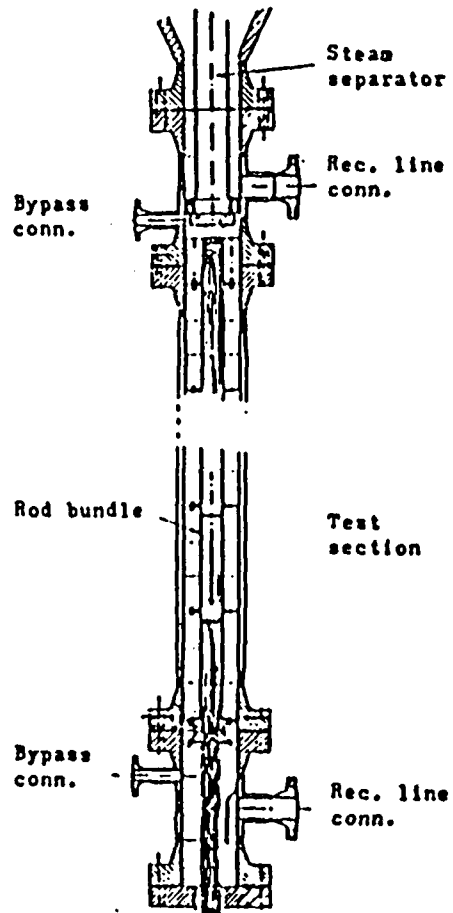


Figure 3.a

Lower plenum and core region.

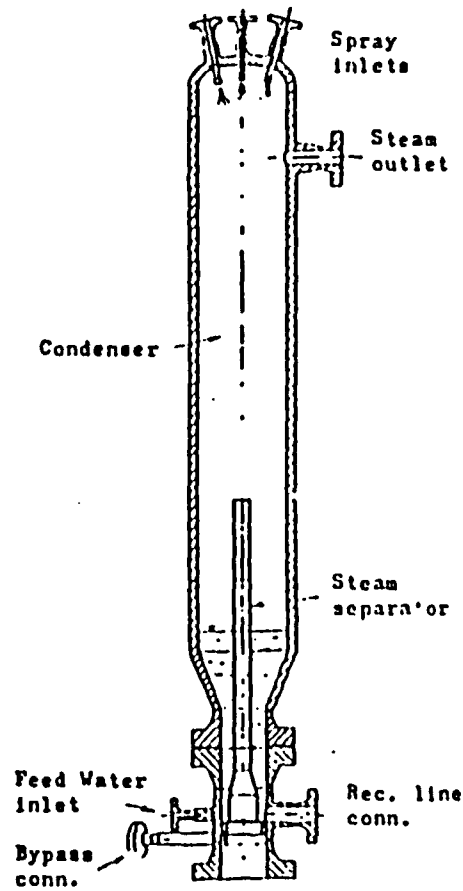


Figure 3.b

Steam separator and steam condenser.

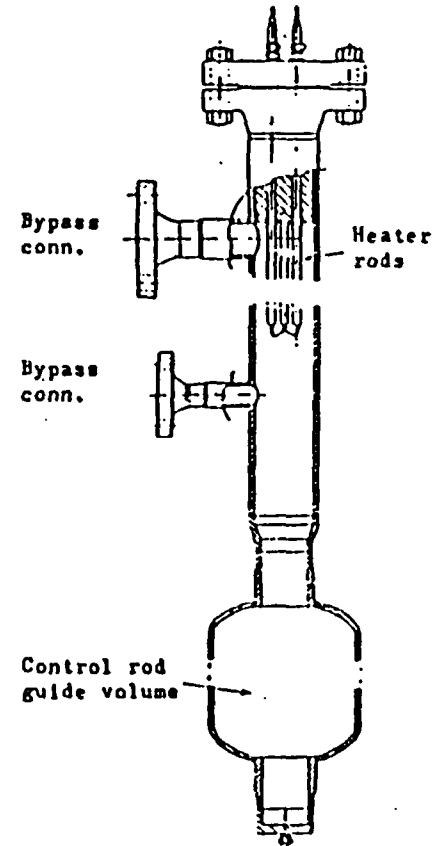


Figure 3.c

The external core bypass.

1986-10-28

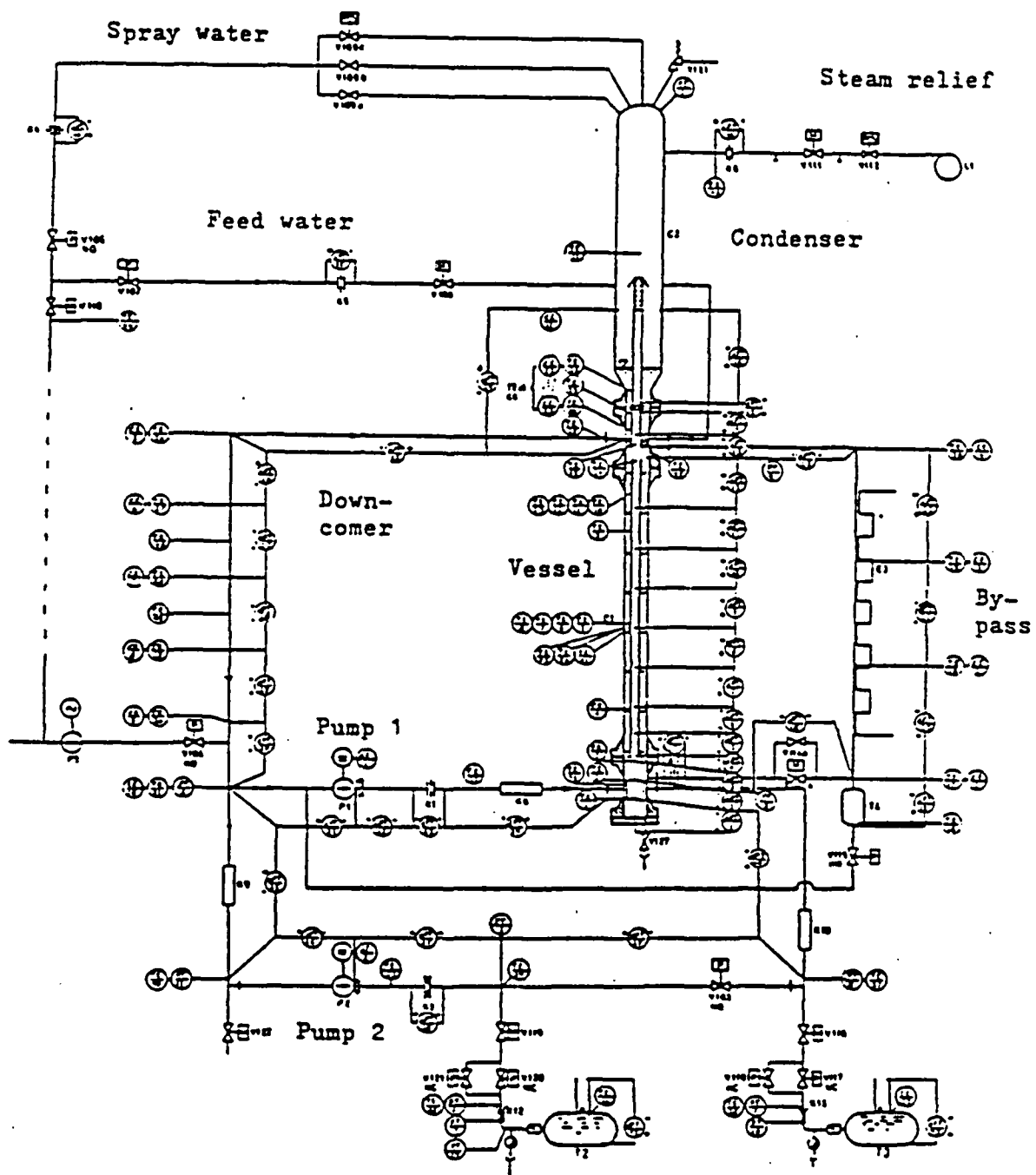


Figure 4

Instrumentation diagram for FIX-II experiment No. 5061.

1986-10-28

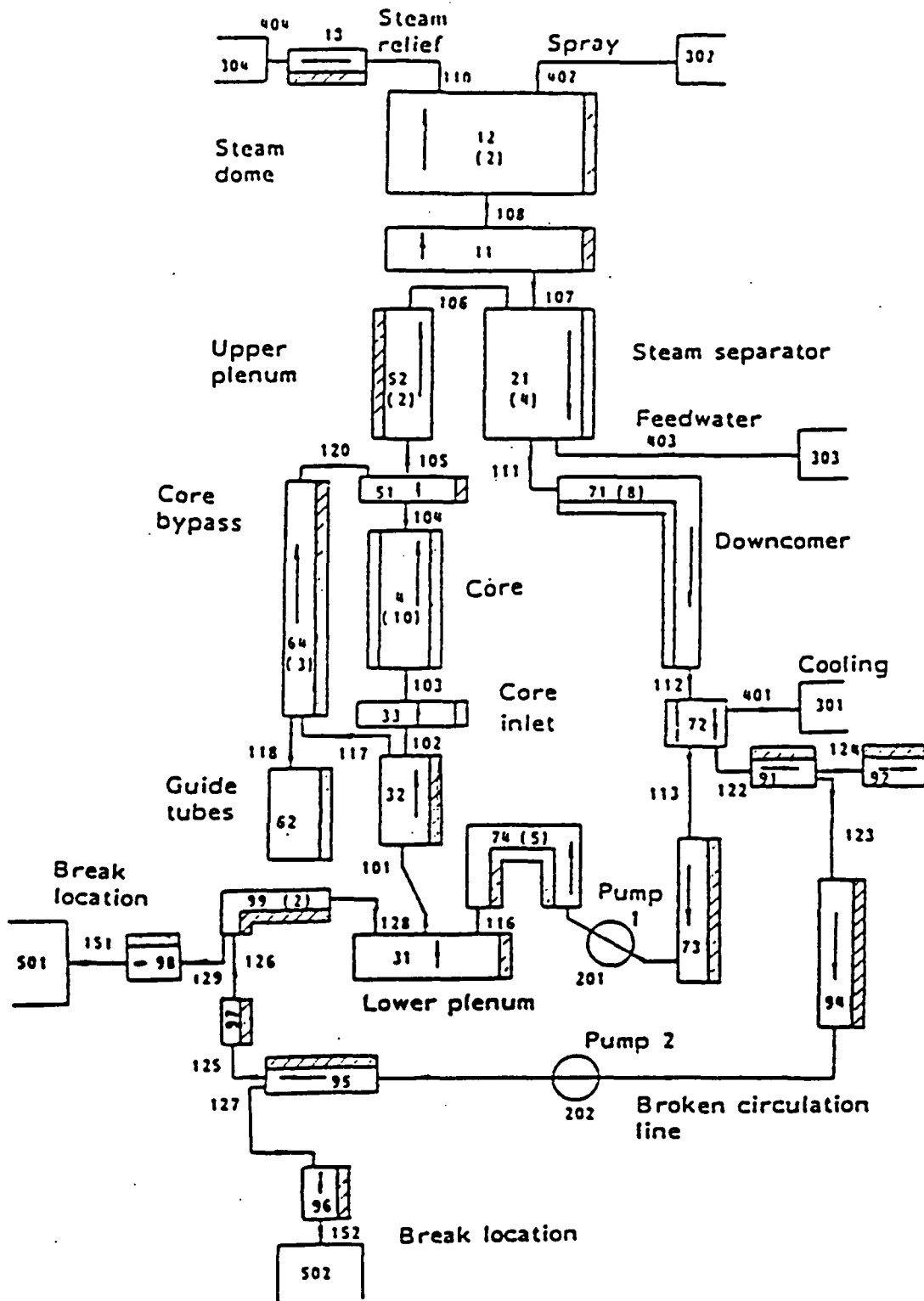


Figure 5

The nodalization diagram for FIX-II experiment No. 5061.

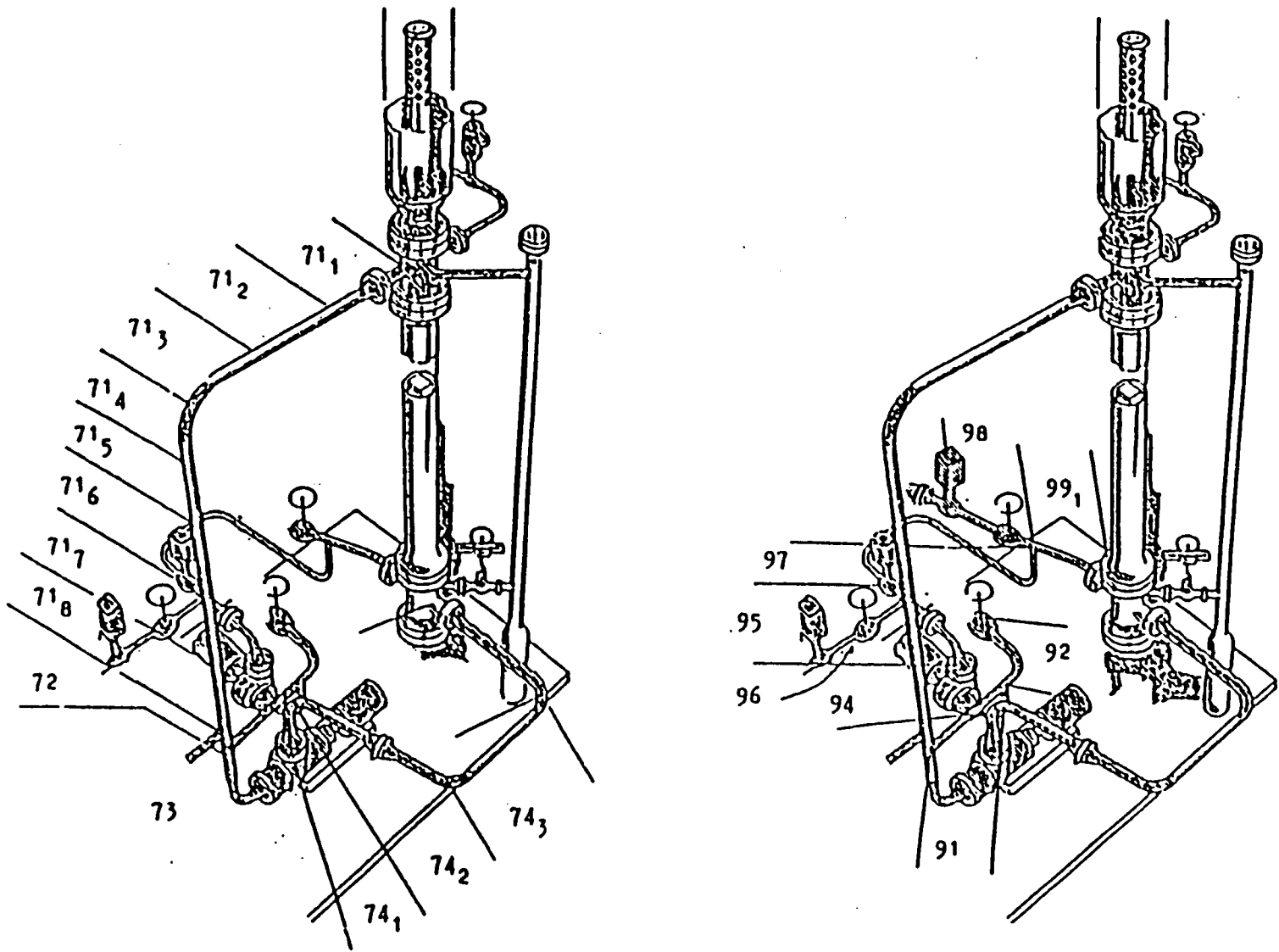


Figure 6
Nodalization of the recirculation lines

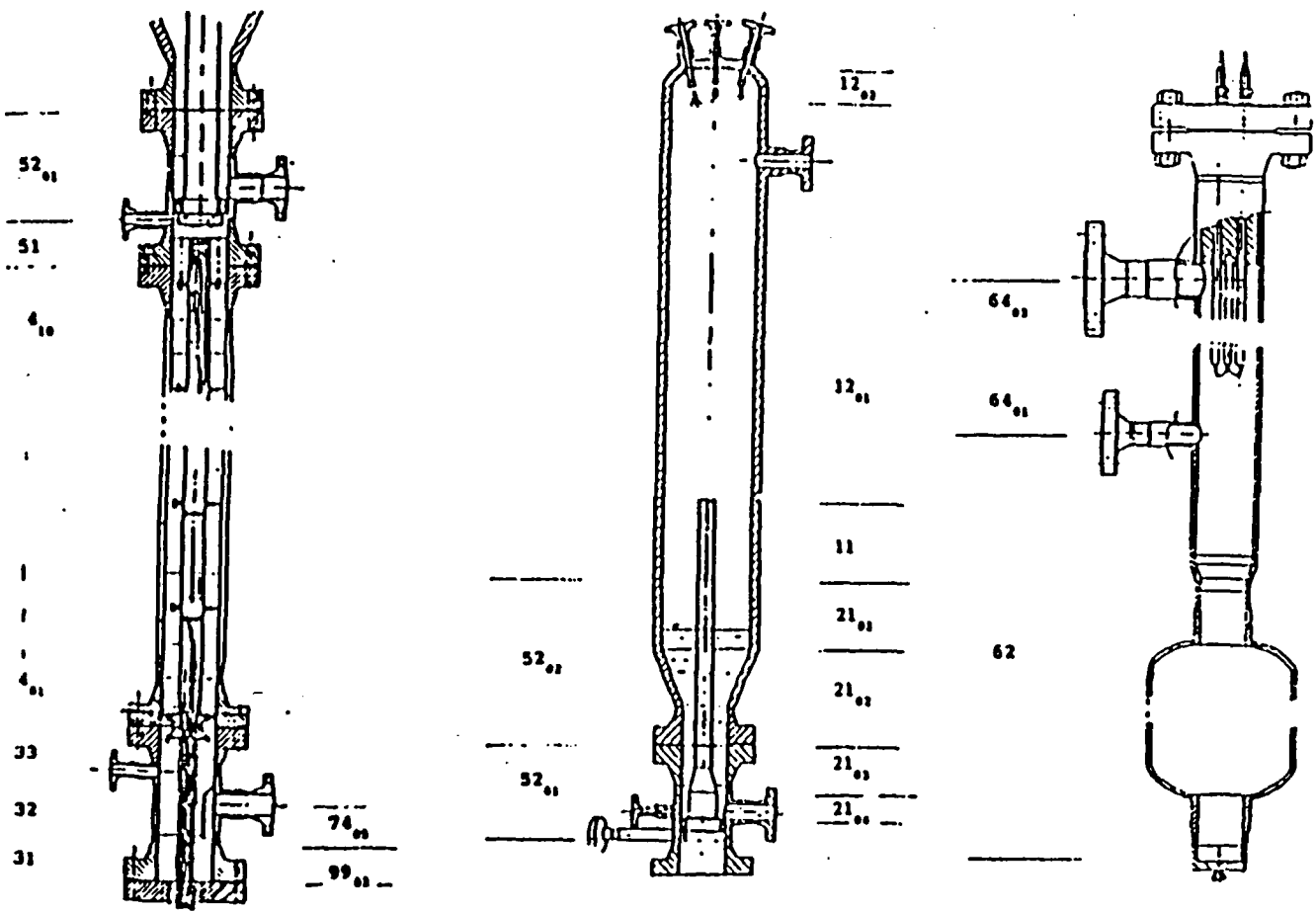


Figure 7

Nodalization of the volumes of the FIX-II
(compare Figure 3).

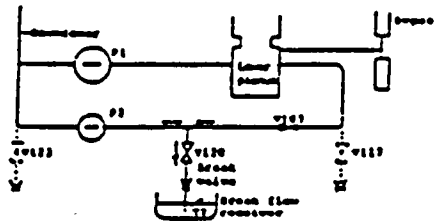
1986-10-28

Table 1

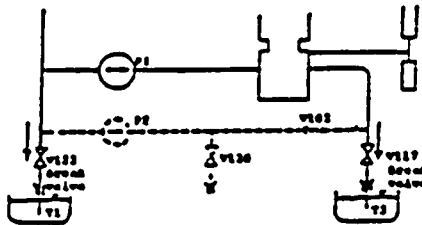
The test matrix for the first FIX-II LOCA experimental period. Test No. 3027 is one matrix No. 2 experiment.

Break classification	Split breaks						Guillotine		
	A						B	C	
Type of simulation (see Figure 13)									
Relative break area (%)	10	31	48	100	150	200	155*	200	
Breaks I.D. (mm)	6.8	12.0	15.0	21.6	26.4	30.5	16.0+ 21.6	21.6+ 21.6	
Initial bundle power (MW)									
-hot channel			3.35	3.35				3.35	
-average	2.35	2.35			2.35	2.35	2.35	2.35	
LOCA test ident. No.	3051	3013	3024 3025 3026 3027	3031	3061	3071	3041	4011 5061	5051 5052

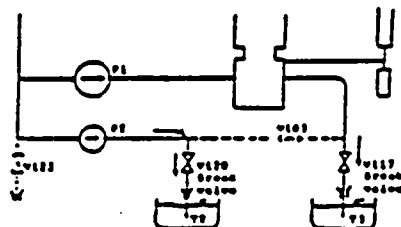
Break type A
Split break



Break type B
Simplified guillotine break



Break type C
Guillotine break



1986-10-28

Table 2.a

Evaluated measurement errors.

Quantity	Probable error	Error corresponding to 95 % confidence level
Pressures	0.014 MPa	0.04 MPa
Fluid temperatures	1°C	2°C
Cladding temperatures	1.6°C	3.2°C
Small range differential pressures (5 to 7.5 kPa)	0.13 kPa	0.3 kPa
Medium range differential pressures (25 to 50 kPa)	0.22 kPa	0.5 kPa
High range differential pressures (100 to 700 kPa)	0.26 kPa	0.65 kPa

Table 2.b

Errors in derived quantities.

Quantity	Probable error
Mass flow rate in orifice meter K1 (P1)	0.2 kg/s
Mass flow rate in orifice meter K2 (P2)	0.14 kg/s
Mass flow rate in orifice meter K6 (steam flow)	-10 % of actual value
Mass flow rate in orifice meter K7 (Bypass)	-10 % of actual value
Break mass flow rate	-10 % of actual value
Electric power to bundle and bypass heaters	1 % of max value

1986-10-28

Table 3

RELAP5/Mod 2 code features.

COMPUTATION PROCESSING FEATURES

- Several problem type and execution control options as
 - a. steady state initialization using fictitious structure heat capacities for faster convergence
 - b. transient calculation
 - c. strip type execution, to select requested parameters from a restart file
 - d. trip system, to decide on actions during calculation due to reaching specified conditions in calculation parameters.
 - e. ability to delete or add hydrodynamic components, structure components and control variables at a restart of calculation.

CLASSIFICATION OF HYDRODYNAMIC MODEL

- One-dimensional, with provisions for
 - a. choked flow model
 - b. abrupt area change model
 - c. cross flow junctions.
- Two-fluid, six equation, space-time numerical solution scheme.
- flow regime oriented field characteristics depending on mass flux and void fraction for
 - a. horizontal flow with bubbly, slug, mist and stratified fields
 - b. vertical flow with bubbly, slug, annular-mist (and stratified) fields
 - c. high mixing flow with bubbly and mist fields (for pumps).

1986-10-28

Table 3 cont'dHYDRODYNAMIC COMPONENTS (Input systematics)

- Volume type components
 - a. single volume
 - b. pipe and annulus, for condensed input of several similar single volumes
 - c. time dependent volume, for defining a boundary source with a time dependent fluid state
 - d. branch, a volume capable of two or more connecting junctions at either end
 - e. pump, characterized by rated values for flow, head, torque, density and moment of inertia. The single phase homologous curve, two-phase multipliers and phase difference tables to model the dynamic pump behaviour
 - f. special system components for steam separator, jetmixer, turbine and accumulator.

- Junction type components
 - a. single junction
 - b. time dependent junction, for a time dependent junction flow with a time dependent or controlled flow state
 - c. cross-flow junction, to model a small cross flow, a tee branch or a small leak flow
 - d. valve, various operation characteristics available for check valve, trip valve, inertial valve and relief valve.

INTERPHASE CONSTITUTIVE EQUATIONS

- Interphase drag
 - a. steady drag due to viscous shear depending on flow regime. Semi-empirical mechanisms to describe flow regime transitions
 - b. dynamic drag due to virtual mass effect.

- Interphase mass and heat transfer depending on flow regime and the fluid fields to saturation temperature differences

1986-10-28

Table 3 cont'dFLUID TO WALL CONSTITUTIVE EQUATIONS

- Wall friction due to wall shear effects formulated for flow regimes and based on a two-phase multiplier approach.
- Wall heat transfer depending on flow characteristics defined for
 - a. single-phase forced convection (Dittus-Boelter)
 - b. saturated nucleate boiling (Chen)
 - c. subcooled nucleate boiling (modified Chen)
 - d. critical heat flux (Biasi or modified Zuber)
 - e. transition film boiling (Chen)
 - f. film boiling (Bromley-Pomeranz and Dougall-Rohsenow)
 - g. condensation (partly Dittus-Boelter).
- Interfacial mass transfer at the wall depending on wall, fluid and saturation temperatures for
 - a. subcooled and saturated boiling
 - b. transition film and film boiling
 - c. condensation.

HEAT STRUCTURES

These may be rectangular, cylindrical or spherical in shape. The structure position is defined through component numbers of left and right hand side hydraulic components. A structure is physically defined by the geometry and the temperature dependent conductivity and volumetric heat capacity data. The structure model is further specified by the number of internal mesh points in the direction of heat flow.

CONTROL COMPONENTS

By these new (control) variables are defined from calculated parameters using algebra, standard functions, trip type operands or integrals.

1986-10-28

Table 4

Initial conditions for test No. 5061.

Quantity		Measured	Predicted			
			Case A	Case B	Case C	Case D
Pressure in the steam dome	(MPa)	6.97	6.97	6.97	6.97	6.97
Power to the 36-rod bundle (incl connections)	(MW)	2.37	2.37	2.37	2.37	2.37
Power to the bypass heaters	(kW)	60.4	60.4	60.4	60.4	60.4
Cooling power in the filler body space	(kW)	234.	232.	233.	233.	233.
Mass flow rate through pump P1	(kg/s)	4.74	4.74	4.74	4.74	4.74
Mass flow rate through pump P2	(kg/s)	1.53	1.53	1.53	1.53	1.53
Mass flow rate in the bypass	(kg/s)	.67	.67	.67	.67	.67
Mass flow rate in the 36-rod bundle	(kg/s)	5.60	5.60	5.60	5.60	5.60
Mass flow rate in the spray line	(kg/s)	3.35	3.35	3.35	3.35	3.35
Mass flow rate in the feed water line	(kg/s)	1.80	1.80	1.80	1.80	1.80
Temperature of water at the bundle inlet	(C)	266.	269.9	269.9	269.8	269.6
Temperature of feed and spray water	(C)	181.	181.8	182.5	182.4	182.6
Water level in the spray condenser	(m)	.898	.897	.892	.895	.898
Rotational speed of pump P1	(/s)	23.72	24.97	24.98	23.40	24.97
Rotational speed of pump P2	(/s)	31.93	32.48	32.50	30.58	32.48
Head of pump P1	(kPa)	112.3	118.3	118.4	103.7	118.3

Table 5

List of events in test No. 5061.

Event	Imposed action	System reaction	Time (s)			
			Case A	Case B	Case C	Case D
The break valve V117 starts to open	.0		.0	.0	.0	.0
Start of coast down of pump P1	.0		.0	.0	.0	.0
Start of power decay in the rod bundle	.0		.0	.0	.0	.0
Flow reversal in the bundle and bypass inlets		.0	.0	.0	.0	.0
The break valve V120 starts to open	.1		.1	.1	.1	.1
The valve V103 in the broken RCL is closed	.3		.3	.3	.3	.3
Start of power decay in the bypass heaters	.3		.3	.3	.3	.3
The SRV starts to open	.7		.7	.7	.7	.7
Dryout occurs		.9	1.	.5	.5	1.
The SRV is fully open	1.2-27.4		1.2-	1.2-	1.2-	1.2-
Flashing starts in the LP (at saturation) *		1.8	5.6	6.3	5.7	6.3
The spray flow is closed	2.2		2.2	2.2	2.2	2.2
The feed water flow is closed	2.3		2.3	2.3	2.3	2.3
Valve V104 to the evaporation cooler is closed	2.3		2.3	2.3	2.3	2.3
Cavitation in pump P1		6.5	5.8	6.7	5.4	7.3
The downcomer is depleted of water (two-phase)		9.	7.9	9.2	8.7	6.9
Flashing starts in the bypass guide tubes volume		10.8	9.5	10.4	10.1	9.5
Core uncover begins		23.	24.	26.	25.	23.
Test stop signal		27.3	-	-	-	-

* Determined from exp. temperature curves and from predicted changes to positive vapor generation.

Abbreviations: LP = Lower plenum
 UP = Upper plenum
 RCL = Recirculation line
 SRV = Steam relief valve

1986-10-28

Table 6

Summary of the main results in test No. 5061.

	Measured	Predicted			
		Case A	Case B	Case C	Case D
Total time of transient (break discharge) (s)	27.8	-	-	-	-
Time to initial dryout (s)	.9	1.0	.5	.5	1.0
Time to beginning of bundle uncovering (s)	23.	24.	26.	25.	23.
Break mass flow 1 s after the break * (kg/s)	33.	30.	31.	35.	34.
Max. break flow rate from lower plenum (kg/s)	19.	22.	22.	24.	26.
Max. break flow rate from the downcomer (kg/s)	14.	-	-	14.	11.
Dome pressure at the end of test (27.4 s) (Mpa)	2.0	12.6	1.7	1.4	1.3
Max. rod dryout temperature (C)	460. (526.)**	487.	463.	489.	408.
Max. rod temperature, end of blowdown (C)	278. (451.)**	244.	227.	227.	234.
Integrated break mass flow (kg)	290.	258.	277.	286.	286.
Integrated steam relief mass flow (kg)	8.	8.6	9.1	8.6	8.4

* Approx. at the maximum break flow of the test

** Max. compared mean temperature. Max. of all exp. measurements put in brackets.

Table 7

Run statistics data (Case C).

Time (s)	Computer CPU time (s)	No. of time steps	No. of time step reductions in interval				
			quality	extrap.	mass	propty.	Courant
-20.	-498.	-320	-	-	-	-	-
0.*	0.	0	0	0	0	0	0
10.	322.	170	0	0	3	0	0
20.	1103.	586	32	0	16	15	149
28.	1562.	858	7	0	5	1	124

* Time of break opening

1986-10-28

Table 8

Parameters used in the assessment comparisons for
FIX-II No. 5061.

COMPONENT	CONTINUOUS PARAMETER *	EXPERIMENT (IDENTIFIER)	PREDICTION (MINOR EDIT)	PLOT IDENTIF. EXP. CALC.	PLOT NO.	
CORE	FLUID DENSITY, BOTTOM	***	RHO 04.01	RH1?	B. 1	
	MASS FLOW RATE, INLET *	DPT 4	P 33.01 - P04.01	D 4 PD4?	B. 2	
	HEATING POWER	X 801	CNTRLVAR 57	X801 HP1?	B. 3	
	CLAD TEMPERATURE, LEVEL 1	TE 191, TE 206, TE 211, TE 246	MTTEMP 4.31000105	TC 1 MT1?	B. 4	
	-"- . LEVEL 3	TE 108, TE 183, TE 243, TE 248	MTTEMP 4.03000105	TC 3 MT2?	B. 5	
	-"- . LEVEL 5	TE 202, TE 227, TE 232, TE 237, TE 252	MTTEMP 4.04000105	TC 5 MT3?	B. 6	
	-"- . LEVEL 7	TE 101, TE 110, TE 114, TE 136, TE 171, TE 186, TE 196, TE 204, TE 210, TE 215, TE 220, TE 235, TE 245, TE 250, TE 258, TE 271	MTTEMP 4.05000105	TC 7 MT4?	B. 7	
	-"- . LEVEL 9	TE 102, TE 137, TE 167, TE 172, TE 187, TE 197, TE 272	MTTEMP 4.06000105	TC 9 MT5?	B. 8	
	-"- . LEVEL 12	TE 118, TE 123, TE 128, TE 148, TE 223	MTTEMP 4.07000105	TC12 MT6?	B. 9	
	-"- . LEVEL 15	TE 175, TE 190, TE 275	MTTEMP 4.10000105	TC15 MT7?	B.10	
	INLET TEMPERATURE	TE 3	TEMPF 33.01	T 3 TF1?	B.11	
	OUTLET TEMPERATURE	TE 14	TEMPF 51.01	T 14 TF2?	B.12	
	CORE INVENTORY *	DPT 5 + DPT 6 + DPT 7 + DPT 8 + DPT 9 + DPT 10 + DPT 11 + DPT 12	P 04.01 - P 51.01 **	D CO POC?	B.13	
	VESSEL	FLUID DENSITY, BOTTOM	***	RHO 31.01	RH2?	B.14
		DOWNCOMER MASS INVENTORY *	DPT 27 + DPT 28 + DPT 29 + DPT 30	P 71.03 - P 72.01 **	D DC PDD?	B.15
LOWER PLENUM MASS INVENTORY *		DP 2 + DP3 - DP 1	P 31.01 - P 32.01 **	D LP PDL?	B.16	
UPPER PLENUM MASS INVENTORY *		DP 13 + DP 14	P 51.01 - P 52.01 **	D UP PDU?	B.17	
PRESSURE LOSS, S.S. ORIFICE		DP 58	P 52.01 - P 52.02	D 58 PDS?	B.18	
DOWNCOMER TEMPERATURE, BOTTOM		TE 31	TEMPF 71.08	T 31 TF3?	B.19	
UPPER PLENUM TEMPERATURE		TE 18	TEMPF 82.01	T 15 TF4?	B.20	
LOWER PLENUM PRESSURE		PT 3	P 31.01	P 3 P 1?	B.21	
UPPER PLENUM PRESSURE		PT 4	P 52.01	P 4 P 2?	B.22	
MASS FLOW RATE, BYPASS		X 602	MFLOWJ 117	X602 MF1?	B.23	
RECIRCULATION LINE		MASS FLOW RATE, I. L. PUMP (ORIFICE K1)	X 603	MFLOWJ 201.02	X603 MF2?	B.24
	MASS FLOW RATE, B. L. PUMP (ORIFICE K2)	X 604	MFLOWJ 202.02	X604 MF3?	B.25	
	MASS FLOW RATE, B. L. VESSEL INLET (SPOOL PIECE K10)	X 610	MFLOWJ 97.02	X610 MF4?	B.26	
SYSTEM	MASS INVENTORY	***	TMASS	MA?	B.27	
	MASS FLOW RATE, STEAM RELIEF	X 607	MFLOWJ 404	X607 MF5?	B.28	
	HEAT LOSS, PASSIVES	***	CNTRLVAR 53	HL1?	B. 3	

1986-10-28

Table 8 cont'd

COMPONENT	CONTINUOUS PARAMETER *	EXPERIMENT (IDENTIFIER)	PREDICTION (MINOR EDIT)	PLOT IDENTIF. EXP. CALC.	PLOT NO.
BREAK	FLUID DENSITY	***	RHO 96.01		RH37 8.29
	MASS FLOW RATE TO T2	X 636	MFLOWJ 152	X636	MF67 8.30
	MASS FLOW RATE TO T3	***	MFLOWJ 151		MF77 8.31
	MASS FLOW RATE, INTEGR. T2	X 661	CNTRLVAR 55	X661	ML17 8.32
	MASS FLOW RATE, INTEGR. T3	***	CNTRLVAR 60		ML27 8.33
	INLET TEMPERATURE	TE 34	TEMPF 96.01	T 34	TF57 8.34
	INLET SUBCOOLING	***	TEMPG 96.01 - TEMPF 96.01		TSU7 8.35
INLET PRESSURE	PT 6	P 96.01	P 6	P 37 8.36	
RELAPS/MOO2	COMPUTATION CPU TIME	***	CPUTIME		CPU7 8.37
	COMPUTATION MASS ERROR	***	EMASS		MAE7 8.38

* THE COMPARISON PARAMETERS ARE THOSE REPORTED AS DIRECTLY MEASURED OR AS COMPUTED RESULTS FROM THE EXPERIMENT.
PRESSURE DIFFERENCE INSTEAD OF MASS FLOW RATE OR OF MASS INVENTORY.

** CORRECTIONS APPLIED TO RESUME THE CORRECT PRESSURE SENSOR LEVELS.

*** NO DATA AVAILABLE FROM THE EXPERIMENT.



Steady state input, Case A

```

* INPUT FOR RELAPS/NTS (OH FILE P14133)
* P14-1) CHILLOTIME BREAK STEADY-STATE TEST NO. 50611
* 300 & SPLIT BREAK
* CASE A
*
0000100 NEW STBY-31
0000101 PLAN
0000102 10. 20.
0000103 30. 1.0E-8 .0475 00001 10 400 400
*
0000200 P 032010000 +PRESSURE LOWER PLENUM VOL 3
0000201 P 004010000 +PRESSURE CORE VOL 1
0000202 P 004100000 +PRESSURE CORE VOL 10
0000203 P 031010000 +PRESSURE UPPER PLENUM
0000204 P 011010000 +PRESSURE STEAM DOME VOL11
0000205 P 011010000 +PRESSURE STEAM DOME VOL12-1
0000206 P 031010000 +PRESSURE DC ANNUBUS VOL 1
0000207 CHTRVAR 041 +LIQUID LEVEL IN DC ANNUBUS
0000208 VALVAREA 000000117 +VALVE AREA BY-PASS INLET
0000209 VOID 004010000 +VOID CORE VOL 1
0000210 VOID 004010000 +VOID CORE VOL 2
0000211 VOID 004010000 +VOID CORE VOL 3
0000212 VOID 004010000 +VOID CORE VOL 4
0000213 VOID 004010000 +VOID CORE VOL 5
0000214 VOID 004010000 +VOID CORE VOL 6
0000215 VOID 004010000 +VOID CORE VOL 7
0000216 VOID 004010000 +VOID CORE VOL 8
0000217 VOID 004010000 +VOID CORE VOL 9
0000218 VOID 004100000 +VOID CORE VOL 10
0000219 VOID 004010000 +VOID BY-PASS INLET
0000220 VOID 032010000 +VOID BEIER TOP
0000221 VOID 011010000 +VOID STEAM DOME VOL11
0000222 VOID 011010000 +VOID STEAM DOME VOL12-1
0000223 VOID 011010000 +VOID STEAM DOME VOL12-2
0000224 VOID 011010000 +VOID DC ANNUBUS VOL 1
0000225 VOID 011010000 +VOID DC ANNUBUS VOL 2
0000226 VOID 011010000 +VOID DC ANNUBUS VOL 3
0000227 VOID 011010000 +VOID DC ANNUBUS VOL 4
0000228 VOID 004010000 +VOID BYPASS VOL 1
0000229 VOID 004010000 +VOID CRID TUBE VOL
0000230 VOID 011010000 +VOID LOWER PLENUM VOL 2
0000231 VOID 011010000 +VOID LOWER PLENUM VOL 1
0000232 VOID 011010000 +VOID BREAK VOLUME
0000233 QUALITY 013010000 +QUALITY STEAM LINE
0000234 VOID 013010000 +VOID PUMP P1 SUCTION LINE
0000235 VOID 014010000 +VOID PUMP P2 SUCTION LINE
0000236 MFLOW 004000000 +MASS FLOW STEAM VALVE
0000237 MFLOW 000000000 +MASS FLOW 33 LEVEL NODE
0000238 MFLOW 110000000 +MASS FLOW STEAM FEEDER
0000239 MFLOW 103000000 +MASS FLOW CORE JUM 1
0000240 MFLOW 004010000 +MASS FLOW CORE JUM 2
0000241 MFLOW 004010000 +MASS FLOW CORE JUM 3
0000242 MFLOW 004010000 +MASS FLOW CORE JUM 4
0000243 MFLOW 004010000 +MASS FLOW CORE JUM 5
0000244 MFLOW 004010000 +MASS FLOW CORE JUM 6
0000245 MFLOW 004010000 +MASS FLOW CORE JUM 7
0000246 MFLOW 004010000 +MASS FLOW CORE JUM 8
0000247 MFLOW 117000000 +MASS FLOW BY-PASS INLET
0000248 MFLOW 170000000 +MASS FLOW BY-PASS OUTLET
0000249 MFLOW 100000000 +MASS FLOW FROM BEIER
0000250 MFLOW 107000000 +MASS FLOW FROM STEAM DOME VOL11
0000251 MFLOW 100000000 +MASS FLOW FROM STEAM DOME VOL12-1
0000252 MFLOW 107010000 +MASS FLOW FROM STEAM DOME VOL12-2
0000253 MFLOW 011010000 +MASS FLOW DC ANNUBUS JUM 1
0000254 MFLOW 011010000 +MASS FLOW DC ANNUBUS JUM 2
0000255 MFLOW 011010000 +MASS FLOW DC ANNUBUS JUM 3

```

```

0000270 MFLOW 201020000 +MASS FLOW PUMP1 OUTLET
0000271 MFLOW 00000201 +PUMP1 VELOCITY (RAD/S)
0000272 MFLOW 202020000 +MASS FLOW PUMP2 OUTLET
0000273 MFLOW 00000202 +PUMP2 VELOCITY (RAD/S)
0000274 CHTRVAR 03 +STRUCTURE HEAT LOSS
0000275 CHTRVAR 04 +STRUCTURE HEAT LOSS INTEGRATED
0000276 CHTRVAR 05 +INTEGRATED BREAK LOSS, T2
0000277 CHTRVAR 06 +DCR-HEAT LOSS
0000278 CHTRVAR 07 +COR-POWER
0000279 CHTRVAR 08 +BY-PASS POWER
0000280 CHTRVAR 09 +TOTAL POWER
0000281 CHTRVAR 042 +LIQUID LEVEL IN UPPER PLENUM
0000282 CHTRVAR 043 +LIQUID LEVEL IN CORE
0000283 CHTRVAR 044 +LIQUID LEVEL IN LOWER PLENUM
0000284 CHTRVAR 00 +INTEGRATED BREAK LOSS, T3
0000285 CHTRVAR 014 +FLOW QUAL CORE VOL 8
0000286 CHTRVAR 016 +FLOW QUAL CORE VOL 8
0000287 CHTRVAR 017 +FLOW QUAL CORE VOL 8
0000288 CHTRVAR 018 +FLOW QUAL CORE VOL 8
0000289 CHTRVAR 019 +FLOW QUAL CORE VOL 8
*
*****
* TRIPS
*
*****
REGULATED STEADY STATE
0000301 TIME 0 GE MALL 0 25. L +STEADY STATE
*
*****
MULTIPLE TRIPS
0000304 TIME 0 GE TIMEOF 001 5. M +TRANSIENT START
0000305 TIME 0 LT MALL 0 0. M
0000306 TIME 0 GE TIMEOF 004 1. M +START OPEN V120
0000307 TIME 0 GE TIMEOF 004 3. M +BYPASS POWER DECA
*
*****
LOGICAL TRIPS
0000401 -S01 AND -S01 M +STEADY STATE
0000402 S01 AND S04 L +TRANSIENT STA
0000403 S04 AND S06 L
0000407 S06 AND S07 L
*
*****
0110000 VOL11 BRANCH
0110001 0
0110101 0.0 1
0110201 0.485 1
0110401 0.0070 1
0110401 00. 1
0110801 0. 1
0111001 00 1
*****
0120000 VOL12 PIPE
0120001 2
0120101 0.0 2
0120501 2.200 1 0.130 2
0120401 0.43700 1 0.02410 2
0120401 00. 2
0120401 00. 1 01 2
0121101 1000 1
*****
0130000 VOL13 SMC1VOL
0130101 0. 3.054 0 01031 0 0. 0 0 0 00
*****
0110000 VOL11 ANNUBUS
0110001 4
0110101 0.0 4
0110201 0. 1 0.035133 2 0. 3
0110301 0.404 1 0.549 2 0.206 3 0.146 4
0110401 0.0710 1 0.0470 2 0.01350 3 0.0017 4
0110401 -10. 4
0110801 0.0390 1 0.0 202 2 0.0 1516 3 0.0 1117 4
0110901 0 0 1 0 96 0 96 2 0 0. 3
0111001 00 4
0111101 1000 3
*****
0110000 VOL11 PIPE
0110001 3
0110101 0.0 3

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Input listings

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0040001 0.01 0 01 2 0 00 0 00 3 0.01 0 01 7 0.06 0 00 0
0040002 0.01 0 01 0
0041001 00 10
0041101 1000 0
*****
0110000 VOL11 BRANCH
0110001 0
0110101 0. 0.100 0.00125 0. 00. 0.100 0. 0.0017 0
*****
0120000 VOL12 PIPE
0120001 2
0120101 0.0 2
0120201 0.001704 1
0120301 0.070 1 0.053 2
0120401 0.0070 1 0.007405 2
0120401 00. 2
0120401 0. 2
0120901 1.70 1.70 1
0121001 00 1
0121101 000 2
*****
0110000 VOL11 ANNUBUS
0110001 4
0110101 0.0 1
0110201 0.485 1
0110401 0.0070 1
0110401 00. 1
0110801 0. 1
0111001 00 1
*****
0120000 VOL12 PIPE
0120001 2
0120101 0.0 2
0120501 2.200 1 0.130 2
0120401 0.43700 1 0.02410 2
0120401 00. 2
0120401 00. 1 01 2
0121101 1000 1
*****
0130000 VOL13 SMC1VOL
0130101 0. 3.054 0 01031 0 0. 0 0 0 00
*****
0110000 VOL11 ANNUBUS
0110001 4
0110101 0.0 4
0110201 0. 1 0.035133 2 0. 3
0110301 0.404 1 0.549 2 0.206 3 0.146 4
0110401 0.0710 1 0.0470 2 0.01350 3 0.0017 4
0110401 -10. 4
0110801 0.0390 1 0.0 202 2 0.0 1516 3 0.0 1117 4
0110901 0 0 1 0 96 0 96 2 0 0. 3
0111001 00 4
0111101 1000 3
*****
0110000 VOL11 PIPE
0110001 3
0110101 0.0 3

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0710101 0.3947 3 0.0198 0
0710101 0.00145 3 0.001725 0
0710101 0. 3 -90 0
0710101 0. 0. 0
0710101 0.00 0.00 2 0.10 0.10 3 0.00 0.00 7
0711001 00 0
0711101 1000 7
*****
0720000 VOL72 BRANCH
0720001 0
0720101 0. 0.300 0.001025 0. -90. -0.300 0. 0. 00
*****
0730000 VOL73 SHCLVOL
0730101 0. 1.248 0.01129 0. -90. -0.768 0. 0. 00
*****
0740000 VOL74 PIPE
0740001 0
0740101 0.00 3
0740201 0. 1 0.001985 3 0. 0
0740301 0.053 1 1.117 3 2.076 3 1.890 4 0.318 2
0740401 0.00740 1 0.00975 2 0.01235 3 0.00923 4 0.00725 5
0740501 90. 1 0 0 -90. 0
0740601 0. 0. 4 0.0015 5
0740701 0.17 0.17 1 0.78 0.78 2 0.22 0.22 3 1.00 1.00 4
0741001 00 0
0741101 1000 1 1000 2 1000 3 1000 4
*****
0820000 VOL82 SHCLVOL
0820101 0. 1.321 0.02227 0. -90. -1.321 0. 0. 00
*****
0840000 VOL84 PIPE
0840001 0
0840101 0.0 3
0840201 1.407 1 1.328 2 1.300 3
0840301 0.01101 1 0.00943 2 0.01187 3
0840401 90. 2
0840501 0. 0.0480 1 0. 0.0472 2 0. 0.0439 3
0840601 0.00 0.00 2
0841001 00 3
0841101 1000 2
*****
BROKEN CIRCULATION LINE
*****
0910000 VOL91 BRANCH
0910001 0
0910101 0. 1.248 0.00170 0. 0. 0. 0. 0. 00
*****
0920000 VOL92 SHCLVOL
0920101 0. 1.320 0.00380 0. 0. 0. 0. 0. 00
*****
0940000 VOL94 SHCLVOL
0940101 0. 1.188 0.00358 0. -45. -0.970 0. 0. 00
*****
0950000 VOL95 BRANCH
0950001 0
0950101 0. 1.690 0.00326 0. 14.3 0.417 0. 0. 00

```

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*****
0960000 VOL96 BRANCH
0960001 0
0960101 0. 1.478 0.00429 0. 0. 0. 0. 0. 00
*****
0970000 VOL97 BRANCH
0970001 0
0970101 0. 3.047 0.00335 0. 4.9 0.161 0. 0. 00
*****
0980000 VOL98 BRANCH
0980001 0
0980101 0. 1.101 0.00450 0. 0. 0. 0. 0. 00
*****
0990000 VOL99 PIPE
0990001 0
0990101 0.0 2
0990201 1.222 1 0.718 2
0990301 0.00787 1 0.00728 2
0990401 0. 1 -90. 2
0990501 0. 0. 1 -0.218 2
0990601 0. 0. 1 0. 0.004812 2
0990701 1.00 1.00 1
0991001 00 2
0991101 1000 1
*****
2010000 PUMP1 PUMP
2010101 0. 0.750 0.01010 0. 10.4 0.783 0
2010106 071010000 0.00417 0.12 0.17 0000
2010109 071000000 0.000100 3.00 3.00 0000
2010201 1 4.74 0. 0.
2010301 1 4.74 0. 0.
2010701 0 0 0 -1 0 0 0
2010102 303.89 0.0268 0.0782 90. 81.7 1. 1000.
2010303 0. 0. 0. 0.
*****
NYA TEKNISKA PUMPKURVOR, DATA KOMMER FRÅN ASEA-ATONS COLIN BER.
O TORQUE FUNKTIONEN SÅRVAR BETYDLIG I DETTA FALL OCH HAR DÄRFÖR INTE
O KONTROLLERATS. KÄLLAN FÖR IN DEL DATA ÄR OKÄND
2011000 1 1
2011101 0.00,1.181 0.27,1.188 0.47,1.160
2011102 0.84,1.130 1.00,1.000
2011200 2 1
2011301 0.00,0.04 0.00,0.07 0.10,0.09
2011302 0.38,0.02 0.55,0.042 0.60,0.09 1.00,1.00
2011300 1 2
2011301 0.0,-0.050 0.41,-0.10 0.01,-0.05 0.70,0.48
2011302 1.00,1.00 2
2011400 1 2
2011401 0.0,-1.16 0.2,0.00 0.60,0.30 1.00,1.00
2011500 1 3
2011501 -1.00,2.00 -0.05,1.01 -0.62,1.52 -0.50,1.39
2011502 0.00,1.10
2011600 1 4
2011601 -1.00,2.00 -0.70,1.52 -0.63,1.25 -0.30,0.93
2011602 0.00,0.72
2011700 2 3
2011701 -1.00,3.31 -0.07,2.78 -0.02,2.29 -0.06,1.95
2011702 -0.37,1.49 -0.22,1.10 -0.10,0.60 0.00,0.00
2011800 2 4
2011801 -1.00,3.31 -0.70,2.78 -0.06,2.27 -0.41,2.04

```

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2012002 -0.21,3.78 0.00,1.95
* TWO PHASE MULTIPLIER TABLES
2013000 0
2013001 0.0,0.0 0.1,0.0 0.15,0.05 0.24,0.0 0.2,0.06 0.4,0.08
2013002 0.0,0.07 0.0,0.0 0.0,0.0 0.06,0.0 1.0,0.0
2013100 0
2013101 0.0,0.0 0.1,0.0 0.16,0.05 0.24,0.0 0.2,0.06 0.4,0.08
2013102 0.0,0.07 0.0,0.0 0.0,0.0 0.06,0.0 1.0,0.0
* TWO PHASE DIFFERENCE FOR PUMP HEAD (SEMICALE)
2014100 1 1
2014101 0.0,0.0 0.1,0.03 0.2,1.00 0.0,1.02 0.7,1.01 0.0,0.04 1.0,1.0
2014200 1 2
2014201 0.0,0.0 0.1,-0.04 0.2,0.0 0.3,0.1 0.4,0.21 0.0,0.61
2014202 0.0,0.00 1.0,1.0
2014300 1 3
2014301 -1.0,-1.16 -0.0,-1.24 -0.0,-1.77 -0.7,-2.36 -0.0,-2.70
2014302 -0.0,-2.91 -0.0,-2.67 -0.25,-1.69 -0.1,-0.5 0.0,0.0
2014400 1 4
2014401 -1.0,-1.16 -0.0,-0.78 -0.0,-0.5 -0.7,-0.31 -0.0,-0.17
2014402 -0.0,-0.00 -0.35,0.0 -0.2,0.01 -0.2,0.00 0.0,0.11
* TWO PHASE DIFFERENCE FOR PUMP TORQUE (= SINGLE PHASE, WHICH MEANS
* THAT FULLY DECREASED TORQUE IS ZERO)
2014900 2 1
2014901 0.00,0.04 0.00,0.07 0.10,0.09
2014902 0.38,0.02 0.60,0.042 0.60,0.09 1.00,1.00
2015000 2 2
2015001 0.0,-1.16 0.5,0.00 0.60,0.30 1.00,1.00
2015100 2 3
2015101 -1.00,3.31 -0.07,2.78 -0.02,2.29 -0.06,1.95
2015102 -0.37,1.49 -0.22,1.10 -0.10,0.60 0.00,0.00
2015200 2 4
2015201 -1.00,3.31 -0.70,2.78 -0.06,2.27 -0.41,2.04
2015202 -0.21,3.78 0.00,1.95
** PUMP1 REGULATOR
2016100 0 CTRLVAR 000
2016101 0. 0 CTRLVAR 1000. 1000.
** PUMP1 CONTROL SYSTEM
20500100 SLIMIT TRIPPOINT 1. 1. 0
20500101 601
*****
20500200 FLOWDIFFE SHM 1. 0. 0
20500201 4.74 -1 0 101020000
*****
20500300 SIGNAL MULT 1. 0. 0
20500301 CTRLVAR 1
20500302 CTRLVAR 2
*****
20500400 INTEGRAL INTEGRAL 80. 150. 0 3 140. 100.
20500401 CTRLVAR 003
*****
20500500 PISPTAB FUNCTION 1. 0. 1
20500501 TIME 0 201
*****
20500600 PIVEL MULT 1. 0. 1
20500601 CTRLVAR 4
20500602 CTRLVAR 5
*****
* PUMP P1 SPEED TABLE
20720100 NTC-1 600 1. 1.
20720101 0. 1.000 4. .785 0. .660 12. .676
20720102 40. .676
*****
0
0
2070000 PUMP2 PUMP

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2020101	0.	0.700	0.00100	0.	77.0	0.770	0					
2020102	0.4410000	0.0010	0.31	0.31	0.000							
2020103	0.0000000	0.000100	3.00	3.00	0.000							
2020104	1	1.53	0.	0.								
2020105	1	1.53	0.	0.								
2020106	0	0	-1	-1	0	0						
2020107	303.69	0.6918	0.01654	29.	13.3	1.	1000.					
2020108	0.	0.	0.	0.								
2021100	1	1										
2021101	0.0	1.136	0.2	1.136	0.4	1.136						
2021102	0.0	1.100	0.8	1.415	1.0	1.000						
2021103	2	1										
2021104	0.0	0.51	1.0	1.00								
2021105	1	1										
2021106	0.0	-0.160	0.3	-0.160	0.4	-0.160	0.0 -0.015					
2021107	0.0	0.145	0.0	0.145	1.0	1.000						
2021108	2	2										
2021109	0.0	-0.47	0.2	-0.21	0.4	0.07						
2021110	0.0	0.35	0.0	0.35	1.0	1.00						
2021111	1	1										
2021112	-1.00	2.00	-0.98	1.01	-0.42	1.53	-0.50	1.38				
2021113	0.00	1.136										
2021114	1	1										
2021115	-1.00	3.00	-0.79	1.53	-0.43	1.35	-0.30	0.93				
2021116	0.00	0.72										
2021117	2	2										
2021118	-1.00	3.31	-0.93	3.70	-0.46	2.33	-0.34	1.95				
2021119	-0.37	1.40	-0.32	1.19	-0.19	0.95	0.00	0.91				
2021120	1	1										
2021121	3	4										
2021122	-1.00	3.31	-0.79	3.70	-0.46	2.37	-0.41	2.04				
2021123	-0.31	1.79	0.00	1.55								
2022000	0											
2022001	0.0	0.00	0.1	0.00	0.2	0.05	0.3	0.00	0.4	0.00	0.6	0.00
2022002	0.0	0.07	0.7	0.00	0.0	0.00	0.0	0.50	1.0	0.00		
2022003	0											
2022004	0.0	0.00	0.1	0.00	0.2	0.15	0.3	0.24	0.4	0.20	0.5	0.40
2022005	0.0	0.10	0.7	0.00	0.0	0.00	0.0	0.50	1.0	1.00		
** PLAMP REGULATOR **STEADY STATE C												
2023100	0											
2023101	0											
** PLAMP CONTROL SYSTEM												
2024000	FLOWDIFF	SLM	1.	0.	0							
2024001	1.53	-1.0										
2025000	SMALL	MAT	1.	0.	0							
2025001	CHIRVAR	1										
2025002	CHIRVAR	2										
2026000	INTEGRAL	INTEGRAL	200.	210.	0	3	170.	230.				
2026001	CHIRVAR	000										
2026100	P3PTAB	FUNCTION	1.	0.	1							
2026101	TIME	0	202									
2026102												
2026103	PWEL	MAT	1.	0.	1							
2026104	CHIRVAR	0										
2026105	CHIRVAR	10										
** PLAMP SPEED TABLE												
2027000	MIC-T	004	1.	1.								
2027001	0.	1.000	2.	.042	2.	.037	0.	.073				
2027002	12.	1.049	10.	1.000	37.	1.103	40.	1.044				

0100000	JUN31-32	SMCL JRM										
0101001	011010000	013000000	0.	0.	0.	0.	0.	1100				
0102001	1	5.27	0.	0.								

0100000	JUN32-33	SMCL JRM										
0101001	012010000	013000000	0.	0.	0.	0.	0.	1100				
0102001	1	5.68	0.	0.								

0100000	JUN33-34	SMCL JRM										
0101001	013010000	004000000	0.000473	0.340	0.200	0.000						
0102001	1	5.68	0.	0.								

0100000	JUN34-35	SMCL JRM										
0101001	004010000	010000000	0.	0.10	0.10	0.100						
0102001	1	4.525	1.078	0.								

0100000	JUN35-37	SMCL JRM										
0101001	013010000	013000000	0.	0.	0.	1100						
0102001	1	9.195	1.078	0.								

0100000	JUN37-38	SMCL JRM										
0101001	012010000	013000000	0.03310	1.	1.	1070						
0102001	1	5.195	1.078	0.								

0100000	JUN38-39	SMCL JRM										
0101001	011000000	013000000	0.0	0.0	0.0	1000						
0102001	1	4.428	-1.078	0.								

0100000	JUN39-40	SMCL JRM										
0101001	013000000	011010000	0.	0.	0.	1000						
0102001	1	4.428	-1.078	0.								

0100000	JUN40-41	SMCL JRM										
0101001	004010000	0101700	2.00	2.00	0.00	0000						
0102001	1	4.5	0.	0.								

0100000	JUN41-42	SMCL JRM										
0101001	012010000	011000000	0.	0.00	0.00	0100						
0102001	1	1.53	0.	0.								

0100000	JUN42-43	SMCL JRM										
0101001	012010000	013000000	0.001433	0.05	0.05	1000	*STEADY 1					
0102001	1	0.	0.	0.								

0100000	JUN43-44	SMCL JRM										
0101001	011010000	011000000	0.	1.00	1.00	1100						
0102001	1	11.42	0.	0.								

0100000	JUN44-45	SMCL JRM										
0101001	011010000	012000000	0.	0.	0.	1000						
0102001	1	11.42	0.	0.								

0100000	JUN45-46	SMCL JRM										
0101001	012010000	013000000	0.00	0.	0.	1000						
0102001	1	4.74	0.	0.								

0100000	JUN46-47	SMCL JRM										
0101001	012010000	011010000	0.	0.00	0.00	1100						
0102001	1	4.74	0.	0.								

0100000	JUN47-48	SMCL JRM										
0101001	012010000	013000000	10.0E-4	12.5	12.5	0000						
0102001	1	1.53	0.	0.								

0100000	JUN48-49	SMCL JRM										
0101001	015010000	016000000	0	1.00	1.00	0100						
0102001	1	0	0.	0.								

0100000	JUN49-50	SMCL JRM										
0101001	011010000	011010000	0.	0.00	0.00	0100						
0102001	1	1.53	0.	0.								

0100000	JUN50-50	SMCL JRM										
0101001	015000000	016000000	0.	1.00	1.00	0100						

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130701 1 0. 0. 0.
*****
o COOLING SYSTEM
*****
3018000 COOLING TMDPVOL
3018101 0.001950 1. 0. 0. 0. 0. 10
3018100 2
3018101 0. 0010000 0.
*****
4010000 COOLING TMDPVOL
4010101 0.77000000 301000000 0.
4010100 1 504
4010101 0. 5.15 0. 0. 2.0 5.15 0. 0. 2.3 0. 0. 0.
*****
3010000 SPRAFFLOW TMDPVOL
3010101 0.001575 1. 0. 0. 00. 1. 0. 0.01575 10
3010100 3 0 CHIRLVAR 30
3010101 452.15 7000000. 452.15
3010102 456.15 7000000. 456.15
*****
4010000 SPRAFFLOW TMDPVOL
4010101 307000000 071010000 0.
4010100 1 504
4010101 0. 3.35 0. 0. 1.0 3.35 0. 0. 2.3 0. 0. 0.
*****
3030000 SUBCOOLING TMDPVOL
3030101 0.000531 1. 0. 0. 0. 0. 0. 10
3030100 3 0 CHIRLVAR 30
3030101 452.15 7000000. 452.15
3030102 456.15 7000000. 456.15
*****
4030000 SUBCOOLING TMDPVOL
4030101 303000000 071010000 0.
4030100 1 504
4030101 0. 1.0000 0. 0. 2.0 1.0000 0. 0. 2.3 0. 0. 0.
*****
o STEAM RELIEF
*****
3040000 RELIEF TMDPVOL
3040101 0.00436 1. 0. 0. 0. 0. 0. 00
3040100 2
3040101 0. 100000. 1.
*****
4040000 RELIEF TMDPVOL
4040101 013010000 304000000 000000
4040100 1 0 CHIRLVAR 100
4040101 0. 0. 0. 0.
4040102 1.55 0. 1.55 0.
*****
o STEAM RELIEF FLOW MODEL
3050100 RWOP MULT 1. 0. 0
3050101 RWOC 013010000 P 013010000
3050100 SOAT POWER 1. 0. 0.

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3050101 CHIRLVAR 03 3
*****
3070100 MORBARZA
3070101 0. 0. .7 0. 1.2 1.
3070102 77 4 1.
*****
3050100 FASTIME TRIPUNIT 1. 0. 1
3050101 501
*****
3030100 RFTIME INTEGRAL 1. 0. 1
3030101 CATALVAR 07
*****
3050100 VALVE AREA FUNCTION 1.031E-4 0. 0
3050101 CHIRLVAR 00 03
*****
3051000 M3FLOW MULT 3547 0. 0
3051001 CHIRLVAR 03 CHIRLVAR 04
*****
*****
o DUMP VOLUMES
*****
3010000 DUMP1 TMDPVOL
3010101 1.00 1.00 0. 0. 0. 0. 0. 00
3010100 3
3010101 0. 100000. 1.0
*****
3020000 DUMP2 TMDPVOL
3020101 1.00 1.00 0. 0. 0. 0. 0. 00
3020100 3
3020101 0. 100000. 1.0
*****
o CHILLTIME RUPTURE IN CIRCULATION LINE
*****
1310000 BARV117 VALVE
1310101 010010000 001000000 0.0003664 0. 0. 0100 1.00 1.00 *017
1310100 1 0. 0.
1310100 MTRVLV
1310101 0000104 0000105 1.00 0.0 *OPENING TIME .30 SEC
*****
1320000 BARV128 VALVE
1320101 010010000 002000000 0.0003664 0. 0. 0100 1.00 1.00 *017
1320100 1 0. 0.
1320100 MTRVLV
1320101 0000106 0000105 1.00 0.0 *OPENING TIME .30 SEC
*****
1330000 VALV103 VALVE
1330101 010010000 007000000 0.0017 0. 0. 0100 1.00 1.00
1330101 1 1.03 0. 0.
1330100 MTRVLV
1330101 0000105 0000104 3.3333 1.0 *CLOSING TIME .30 SEC
*****
o HEAT STRUCTURES
14010000 1 7 2 1 0. *CORE
14010100 0 4
14010101 4 0.001725 2 0.006125
14010101 1 4 -2 5
14010101 0 0 4 1 0 0
14010400 0
14010401 570. 7
14010501 0 0 0 0 1 13.240 1
14010601 004010000 0 1 1 13.240 1

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14010701 1 0 0164 0. 0. 1
14010901 0 0 01747 0. 0. 1
14020000 1 7 2 1 0.
14020100 0 1
14020101 4 0.001975 2 0.006125
14020201 1 4 -2 5
14020301 0 0 4 1 0 0
14020400 4010
14020501 0 0 0 0 1 13.240 1
14020601 004010000 0 1 1 13.240 1
14020701 1 0 1030 0. 0. 1
14020901 0 0 01747 0. 0. 1
14030000 1 7 2 1 0.
14030100 0 1
14030101 4 0.001975 2 0.006125
14030201 1 4 -2 5
14030301 0 0 4 1 0 0
14030400 4010
14030501 0 0 0 0 1 13.240 1
*****
14040601 004010000 0 1 1 13.240 1
14040701 1 0 1130 0. 0. 1
14040901 0 0 01747 0. 0. 1
14040000 1 7 2 1 0.
14040100 0 1
14040101 4 0.001975 2 0.006125
14040201 1 4 -2 5
14040301 0 0 4 1 0 0
14040400 4010
14040501 0 0 0 0 1 13.240 1
14040601 004010000 0 1 1 13.240 1
14040701 1 0 1130 0. 0. 1
14040901 0 0 01747 0. 0. 1
14050000 1 7 2 1 0.
14050100 4010
14050100 4010
14050400 004010000 0 1 1 13.240 1
14050501 0 0 0 0 1 13.240 1
14050601 004010000 0 1 1 13.240 1
14050701 1 0 1130 0. 0. 1
14050901 0 0 01747 0. 0. 1
14060000 1 7 2 1 0.
14060100 4010
14060400 004010000 0 1 1 13.240 1
14060501 0 0 0 0 1 13.240 1
14060601 004010000 0 1 1 13.240 1
14060701 1 0 1133 0. 0. 1
14060901 0 0 01747 0. 0. 1
14070000 1 7 2 1 0.
14070100 4010
14070400 004010000 0 1 1 13.240 1
14070501 0 0 0 0 1 13.240 1
14070601 004010000 0 1 1 13.240 1
14070701 1 0 1130 0. 0. 1
14070901 0 0 01747 0. 0. 1
14080000 1 7 2 1 0.
14080100 4010
14080400 004010000 0 1 1 13.240 1
14080501 0 0 0 0 1 13.240 1
14080601 004010000 0 1 1 13.240 1
14080701 1 0 1034 0. 0. 1
14080901 0 0 01747 0. 0. 1
14090000 1 7 2 1 0.
14090100 0 1
14090101 4 0.001975 2 0.006125
14090201 1 4 -2 5

```

14090301	0 0 4	1 0 6		
14090400	4010			
14090501	0 0 0	0 1 1	13.248	1
14090601	004030000	0 1 1	13.248	1
14090701	1 0 0017	0 0 0		1
14090801	0 0 01742	0 0 0		1
14100000	1 7 2	1 0 0		
14100100	0 1			
14100201	0 0 003825	2 0 006123		
14100301	1 4	2 5		
14100400	0 0 4	1 0 6		
14100501	4010			
14100601	0 0 0	0 1 1	13.248	1
14100701	004100000	0 1 1	13.248	1
14100801	1 0 0514	0 0 0		1
14100901	0 0 01742	0 0 0		1
10440000	1 2 2	1 0 0	BY PASS	
10440100	0 1			
10440201	1 0 006123			
10440301	2 1			
10440400	1 0 1			
10440501	570. 3			
10440601	0 0 0	0 1 1	2.67	1
10440701	044010000	0 1 1	2.67	1
10440801	2 0 35	0 0 0		1
10440901	0 0 0			1
10450000	0 0 0	0 1 1	2.67	1
10450100	0440			
10450201	0 0 0	0 1 1	2.67	1
10450301	044020000	0 1 1	2.67	1
10450401	2 0 40	0 0 0		1
10450501	0 0 01742	0 0 0		1
10450601	1 2 2	1 0 0		
10450701	0440			
10450801	0440			
10450901	0 0 0	0 1 1	2.67	1
10460001	044030000	0 1 1	2.67	1
10460101	2 0 27	0 0 0		1
10460201	0 0 01742	0 0 0		1

BOX WALL TO ACCOUNT FOR HEAT LOSSES

14000000	10 2 1	1 0 0		
14000100	0 1			
14000201	1 0 002			
14000301	3 1			
14000401	0 1			
14000501	450. 1			
14000601	540. 2			
14000701	-401	-1 3400	0 0 18	10
14000801	004010000	010000	1 0 0 18	10
14000901	0 0 0	0 10		
14001001	0 0 0	0 10		

GENERAL TABLE GIVING HEAT TRANSFER COEFF. AT OUTSIDE OF BOX WALL.
 20240000 HTC-Y
 20240001 0. 2.040003 HTC DETERMINED TO GIVE HEAT LOSS OF APPROX. 2

GENERAL TABLES GIVING THE TEMPERATURES AT THE OUTSIDE OF THE BOX WALL. TEMPERATURE IS SUPPOSED TO VARY LINEARLY BETWEEN 403 K

AT INLET TO 403 K AT OUTLET.

20240100	TEMP			
20240101	0.	407.5		
20240200	TEMP			
20240201	0.	410.0		
20240300	TEMP			
20240301	0.	415.5		
20240400	TEMP			
20240401	0.	434.5		
20240500	TEMP			
20240501	0.	443.5		
20240600	TEMP			
20240601	0.	452.0		
20240700	TEMP			
20240701	0.	461.5		
20240800	TEMP			
20240801	0.	470.5		
20240900	TEMP			
20240901	0.	479.5		
20241000	TEMP			
20241001	0.	488.5		
13100000	1 4 1	1 0 00		
13100100	0 2			
13100201	0.005	1 0 015 2 0 00 3		
13100301	3 3			
13100401	0 2			
13100501	560. 4			
13100601	13010000	0 1 0 170 1		
13100701	-13 0 3014	0 1 170 1		
13100801	0 0 0 0 1			
13100901	0 0 0 0 1			
13200000	1 0 2 1	1 132		
13200100	0 2			
13200201	0.005	1 0 015 2 0 01 3		
13200301	3 3			
13200401	0 2			
13200501	560. 4			
13200601	13010000	0 1 1 325 1		
13200701	-13 0 3014	1 325 1		
13200801	0 0 0 0 1			
13200901	0 0 0 0 1			
13300000	1 4 2 1	1 132		
13300100	0 2			
13300201	0.005	1 0 015 2 0 03 3		
13300301	3 3			
13300401	0 2			
13300501	560. 4			
13300601	13010000	0 1 1 371 1		
13300701	-13 0 3014	1 371 1		
13300801	0 0 0 0 1			
13300901	0 0 0 0 1			

15100000	1 3 2 1	1 132		
15100100	0 1			
15100201	2 162			
15100301	3 2			
15100401	0 2			
15100501	560. 3			
15100601	13010000	0 1 1 170 1		
15100701	-13 0 3014	1 170 1		
15100801	0 0 0 0 1			
15100901	0 0 0 0 1			
15210000	1 3 2 1	1 063		
15210100	0 1			
15210201	2 065			
15210301	3 2			
15210401	0 2			
15210501	560. 3			
15210601	13010000	0 1 1 437 1		
15210701	-13 0 3014	1 437 1		
15210801	0 0 0 0 1			
15210901	0 0 0 0 1			
15220000	1 3 2 1	1 050		
15220100	0 1			
15220201	2 052			
15220301	3 2			
15220401	0 2			
15220501	560. 3			
15220601	13010000	0 1 1 953 1		
15220701	-13 0 3014	1 953 1		
15220801	0 0 0 0 1			
15220901	0 0 0 0 1			
11100000	1 4 2 1	1 350		
11100100	0 2			
11100201	0.005	1 0 015 2 0 033 3		
11100301	3 3			
11100401	0 2			
11100501	560. 4			
11100601	13010000	0 1 1 450 1		
11100701	-13 0 3014	1 450 1		
11100801	0 0 0 0 1			
11100901	0 0 0 0 1			
11210000	1 4 2 1	1 350		
11210100	0 2			
11210201	0.005	1 0 015 2 0 033 3		
11210301	3 3			
11210401	0 2			
11210501	560. 4			
11210601	13010000	0 1 1 2700 1		
11210701	-13 0 3014	1 2700 1		
11210801	0 0 0 0 1			
11210901	0 0 0 0 1			
11220000	1 4 2 1	1 0 00		
11220100	0 2			
11220201	0.005	1 0 015 2 0 033 3		
11220301	3 3			
11220401	0 2			
11220501	560. 4			
11220601	13010000	0 1 0 400 1		
11220701	-13 0 3014	0 400 1		
11220801	0 0 0 0 1			
11220901	0 0 0 0 1			

```

1170601 0 0 0 0 1
0
1110000 1 4 2 1 .250
1110100 0 2
1110101 0.005 1 0.016 2 0.033 3
1110201 3 2
1110301 .0 2
1110401 560. 4
1110501 21010000 0 1 1 .404 1
1110601 -13 0 3014 1 .404 1
1110701 0 .0 .0 .0 1
1110801 0 .0 .0 .0 1
0
1112000 1 4 2 1 .170
1112010 0 2
1112011 0.005 1 0.016 2 0.033 3
1112021 3 2
1112031 .0 2
1112041 560. 4
1112051 21020000 0 1 1 .549 1
1112061 -13 0 3014 1 .549 1
1112071 0 .0 .0 .0 1
1112081 0 .0 .0 .0 1
0
1113000 1 4 2 1 .132
1113010 0 2
1113011 0.005 1 0.016 2 0.01 3
1113021 3 2
1113031 .0 2
1113041 560. 4
1113051 21030000 0 1 1 .286 1
1113061 -13 0 3014 1 .286 1
1113071 0 .0 .0 .0 1
1113081 0 .0 .0 .0 1
0
1114000 1 4 2 1 .132
1114010 0 2
1114011 0.005 1 0.016 2 0.01 3
1114021 3 2
1114031 .0 2
1114041 560. 4
1114051 21040000 0 1 1 .146 1
1114061 -13 0 3014 1 .146 1
1114071 0 .0 .0 .0 1
1114081 0 .0 .0 .0 1
0
1110000 0 3 2 1 .0540
1110010 0 1
1110011 2 .0707
1110021 3 2
1110031 .0 2
1110041 560. 3
1110051 21010000 010000 1 1 0.998 3
1110052 21040000 010000 1 1 0.928 8
1110061 -13 0 3014 1 0.998 3
1110062 -13 0 3014 1 0.928 8
1110071 0 .0 .0 .0 0
1110081 0 .0 .0 .0 0
0
1120000 1 3 2 1 .0540
1120010 0 1
1120011 2 .0707
1120021 3 2
1120031 .0 2
1120041 560. 3

```

```

17200501 22010000 0 1 1 .300 1
17200601 -13 0 3014 1 .300 1
17200701 0 .0 .0 .0 1
17200801 0 .0 .0 .0 1
0
1730000 1 3 2 1 0540
17300100 0 1
17300101 2 .0707
17300201 3 2
17300301 .0 2
17300401 560. 3
17300501 23010000 0 1 1 .716 1
17300601 -13 0 3014 1 .716 1
17300701 0 .0 .0 .0 1
17300801 0 .0 .0 .0 1
0
1740000 4 3 3 1 0360
17400100 0 1
17400101 2 .0445
17400201 3 2
17400301 .0 2
17400401 560. 3
17400501 24010000 0 1 1 .873 1
17400502 24020000 0 1 1 1.117 2
17400503 24030000 0 1 1 2.874 3
17400504 24040000 0 1 1 1.560 4
17400601 -13 0 3014 1 .873 1
17400602 -13 0 3014 1 1.117 2
17400603 -13 0 3014 1 2.874 3
17400604 -13 0 3014 1 1.560 4
17400701 0 .0 .0 .0 4
17400801 0 .0 .0 .0 4
0
1749000 1 3 1 1 0.00
17490100 0 1
17490101 2 .003
17490201 3 2
17490301 .0 2
17490401 560. 3
17490501 24050000 0 1 0 .055 1
17490601 -13 0 3014 0 .055 1
17490701 0 .0 .0 .0 1
17490801 0 .0 .0 .0 1
0
1810000 1 3 2 1 .0678
18100100 0 1
18100101 2 .0695
18100201 3 2
18100301 .0 2
18100401 560. 3
18100501 62010000 0 1 1 1.331 1
18100601 0 .0 .0 .0 1
18100701 0 .0 .0 .0 1
18100801 0 .0 .0 .0 1
0
1840000 3 3 2 1 0486
18400100 0 1
18400101 2 .0572
18400201 3 2
18400301 .0 2
18400401 560. 3
18400501 64010000 0 1 1 1.440 1
18400502 64020000 0 1 1 1.335 2
18400503 64030000 0 1 1 1.363 3
18400601 -13 0 3014 1 1.440 1

```

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18400402 -13 0 3014 1 1.335 2
18400403 -13 0 3014 1 1.363 3
18400701 0 .0 .0 .0 3
18400801 0 .0 .0 .0 3
0
1810000 1 3 2 1 .0360
18100100 0 1
18100101 2 .0445
18100201 3 2
18100301 .0 2
18100401 560. 3
18100501 61010000 0 1 1 1.246 1
18100601 -13 0 3014 1 1.246 1
18100701 0 .0 .0 .0 1
18100801 0 .0 .0 .0 1
0
1820000 1 3 2 1 .0360
18200100 0 1
18200101 2 .0445
18200201 3 2
18200301 .0 2
18200401 560. 3
18200501 62010000 0 1 1 1.339 1
18200601 -13 0 3014 1 1.339 1
18200701 0 .0 .0 .0 1
18200801 0 .0 .0 .0 1
0
1840000 1 3 2 1 .0746
18400100 0 1
18400101 2 .0301
18400201 3 2
18400301 .0 2
18400401 560. 3
18400501 64010000 0 1 1 1.475 1
18400601 -13 0 3014 1 1.475 1
18400701 0 .0 .0 .0 1
18400801 0 .0 .0 .0 1
0
1850000 1 3 2 1 .0746
18500100 0 1
18500101 2 .0301
18500201 3 2
18500301 .0 2
18500401 560. 3
18500501 65010000 0 1 1 1.683 1
18500601 -13 0 3014 1 1.683 1
18500701 0 .0 .0 .0 1
18500801 0 .0 .0 .0 1
0
1860000 1 3 2 1 .0360
18600100 0 1
18600101 2 .0445
18600201 3 2
18600301 .0 2
18600401 560. 3
18600501 66010000 0 1 1 1.475 1
18600601 0 .0 .0 .0 1
18600701 0 .0 .0 .0 1
18600801 0 .0 .0 .0 1
0
1870000 1 3 2 1 .0746
18700100 0 1
18700101 2 .0301
18700201 3 2
18700301 .0 2

```



```

18700401 540. 3
18700501 27010000 0 1 1 3.062 1
18700601 -13 0 2014 0 1 3.062 1
18700701 0 .0 .0 .0 1
18700801 0 .0 .0 .0 1
18400000 1 3 2 1 .0406
18900100 0 1
18900101 2 .0406
18900201 3 2
18900301 .0 2
18900401 560. 3
18900501 27010000 0 1 1 1.181 1
18900601 0 .0 .0 .0 1
18900701 0 .0 .0 .0 1
18900801 0 .0 .0 .0 1
18910000 1 3 2 1 .0406
18910100 0 1
18910101 2 .050
18910201 3 2
18910301 .0 2
18910401 560. 3
18910501 27010000 0 1 1 1.470 1
18910601 -13 0 2014 1 1.470 1
18910701 0 .0 .0 .0 1
18910801 0 .0 .0 .0 1
18920000 1 3 1 1 0.00
18920100 0 1
18920101 2 .003
18920201 3 2
18920301 .0 2
18920401 560. 3
18920501 27010000 0 1 0 .055 1
18920601 -13 0 2014 0 .055 1
18920701 0 .0 .0 .0 1
18920801 0 .0 .0 .0 1
19010000 1 3 1 1 0.00
19010100 0 1
19010101 2 .070
19010201 3 2
19010301 .0 2
19010401 560. 3
19010501 27010000 0 1 0 0.50 1
19010601 -13 0 2014 0 0.50 1
19010701 0 .0 .0 .0 1
19010801 0 .0 .0 .0 1
19020000 1 3 1 1 0.00
19020100 0 1
19020101 2 .070
19020201 3 2
19020301 .0 2
19020401 560. 3
19020501 27010000 0 1 0 0.300 1
19020601 -13 0 2014 0 0.30 1
19020701 0 .0 .0 .0 1
19020801 0 .0 .0 .0 1
1910300 3 5 2 1 0.
19110100 0 1
19110101 2 0.0045 2 0.0070
19110201 1 3 4 5

```

* COPPER RODS

```

19110301 0.0 5
19110400 0
19110401 570. 8
19110501 0 0 0 1 5.00 1
19110502 0 0 0 1 11.70 1
19110503 0 0 0 1 5.00 1
19110504 0 0 0 1 11.70 1
19110601 0 0 0 1 5.00 1
19110602 0 0 0 1 11.70 1
19110603 0 0 0 1 5.00 1
19110701 0 0 0 1 5.00 1
19110801 0 0 0 1 11.70 1
19110901 00 0.01742 0. 0. 1
19110902 1 1 2 1 0. * COPPER CABLES
19111000 0 1
19111001 0 0.004
19111002 4 4
19111003 0.0 4
19111004 0
19111005 570. 8
19111006 0 0 0 1 7.00 1
19111007 0 0 0 1 7.00 1
19111008 0 0 0 1 7.00 1
19111009 00 0.01742 0. 0. 1
19111010 0

```

```

20100100 TML/YCTM 1 -1 0 MG 0
20100101 0. 0.00 472. 0.50 873. 4.64 873. 3.78
20100102 775. 2.10 873. 2.75 873. 2.50 1073. 7.30
20100103 3300000. 3300000. 3300000. 3370000.
20100104 3400000. 3430000. 3717000.
20100200 TML/YCTM 2 2 0 INCHES 000
20100201 293. 1088. 10.034 0.0122 0.000002042 0. 0. 0.
20100202 293. 1088. 265370. 4173.0 -1.7362 0. 0. 0. 0.
20100300 0-STEEL
20100400 TML/YCTM 1 1 0 COPPER
20100401 390. 0
20100402 3.48E+06
20100500 0

```

```

* CORE POWER REDUCTION
20700100 POWER 804 1. 2 370E6
20700101 0.00 1.000 0.40 0.005 1.00 0.037 2.50 0.000 0.00 0.492
20700102 7.50 0.355 10.0 0.341 12.0 0.160 13.0 0.127 20.0 0.043
20700103 25.00 0.043 30.00 0.010 30.00 0.060
* BY-PASS POWER REDUCTION
20700200 POWER 807 1. 60.4E3
20700201 0. 1.000 1.00 0.501 1.00 0.490 2.75 0.0 100. 0.0
20700300 0

```

```

* LIQUID LEVEL IN SOME BC ANNULUS AND DOWNCOMER TO BREAK
HEIGHT OF LIQUID - FCT OF LIQUID VOID
20101100 NORMAREA 0VOL21-2
20101101 0. 0. .380 .3740 1.0 0.540
20101200 NORMAREA 0VOL21-3
20101201 0. 0. 0.490 0.150 1.0 0.206
20701300 TEMP
20701301 0. 390.
20701400 MIC-V
20701401 0. 18.00 *AUXILIARY HEAT TRANSFER COEFF. TO QUIT

```

```

* FLOWS THROUGH SS-JUN 405 AND 406
20501100 L10M21-2 FUNCTION 1. 0. 1
20501101 VOIDF 02103000 011
20501200 L10M21-3 FUNCTION 1. 0. 1
20501201 VOIDF 02103000 011
20501300 L10M21-4 FUNCTION 1. 0. 1
20501301 VOIDF 02103000 011
20501400 L10M21-5 FUNCTION 1. 0. 1
20501401 VOIDF 02103000 011
20501500 L10M21-6 FUNCTION 1. 0. 1
20501501 VOIDF 02103000 011
20501600 L10M21-7 FUNCTION 1. 0. 1
20501601 VOIDF 02103000 011
20501700 L10M21-8 FUNCTION 1. 0. 1
20501701 VOIDF 02103000 011
20501800 L10M21-9 FUNCTION 1. 0. 1
20501801 VOIDF 02103000 011
20501900 L10M21-10 FUNCTION 1. 0. 1
20501901 VOIDF 02103000 011
20502000 L10M21-11 FUNCTION 1. 0. 1
20502001 VOIDF 02103000 011
20502100 L10M21-12 FUNCTION 1. 0. 1
20502101 VOIDF 02103000 011
20502200 L10M21-13 FUNCTION 1. 0. 1
20502201 VOIDF 02103000 011
20502300 L10M21-14 FUNCTION 1. 0. 1
20502301 VOIDF 02103000 011
20502400 L10M21-15 FUNCTION 1. 0. 1
20502401 VOIDF 02103000 011
20502500 L10M21-16 FUNCTION 1. 0. 1
20502501 VOIDF 02103000 011
20502600 L10M21-17 FUNCTION 1. 0. 1
20502601 VOIDF 02103000 011
20502700 L10M21-18 FUNCTION 1. 0. 1
20502701 VOIDF 02103000 011
20502800 L10M21-19 FUNCTION 1. 0. 1
20502801 VOIDF 02103000 011
20502900 L10M21-20 FUNCTION 1. 0. 1
20502901 VOIDF 02103000 011
20503000 L10M21-21 FUNCTION 1. 0. 1
20503001 VOIDF 02103000 011
20503100 L10M21-22 FUNCTION 1. 0. 1
20503101 VOIDF 02103000 011
20503200 L10M21-23 FUNCTION 1. 0. 1
20503201 VOIDF 02103000 011
20503300 L10M21-24 FUNCTION 1. 0. 1
20503301 VOIDF 02103000 011
20503400 L10M21-25 FUNCTION 1. 0. 1
20503401 VOIDF 02103000 011
20503500 L10M21-26 FUNCTION 1. 0. 1
20503501 VOIDF 02103000 011
20503600 L10M21-27 FUNCTION 1. 0. 1
20503601 VOIDF 02103000 011
20503700 L10M21-28 FUNCTION 1. 0. 1
20503701 VOIDF 02103000 011
20503800 L10M21-29 FUNCTION 1. 0. 1
20503801 VOIDF 02103000 011
20503900 L10M21-30 FUNCTION 1. 0. 1
20503901 VOIDF 02103000 011
20504000 L10M21-31 FUNCTION 1. 0. 1
20504001 VOIDF 02103000 011
20504100 L10M21-32 FUNCTION 1. 0. 1
20504101 VOIDF 02103000 011
20504200 L10M21-33 FUNCTION 1. 0. 1
20504201 VOIDF 02103000 011
20504300 L10M21-34 FUNCTION 1. 0. 1
20504301 VOIDF 02103000 011
20504400 L10M21-35 FUNCTION 1. 0. 1
20504401 VOIDF 02103000 011
20504500 L10M21-36 FUNCTION 1. 0. 1
20504501 VOIDF 02103000 011
20504600 L10M21-37 FUNCTION 1. 0. 1
20504601 VOIDF 02103000 011
20504700 L10M21-38 FUNCTION 1. 0. 1
20504701 VOIDF 02103000 011
20504800 L10M21-39 FUNCTION 1. 0. 1
20504801 VOIDF 02103000 011
20504900 L10M21-40 FUNCTION 1. 0. 1
20504901 VOIDF 02103000 011
20505000 L10M21-41 FUNCTION 1. 0. 1
20505001 VOIDF 02103000 011
20505100 L10M21-42 FUNCTION 1. 0. 1
20505101 VOIDF 02103000 011
20505200 L10M21-43 FUNCTION 1. 0. 1
20505201 VOIDF 02103000 011
20505300 L10M21-44 FUNCTION 1. 0. 1
20505301 VOIDF 02103000 011
20505400 L10M21-45 FUNCTION 1. 0. 1
20505401 VOIDF 02103000 011
20505500 L10M21-46 FUNCTION 1. 0. 1
20505501 VOIDF 02103000 011
20505600 L10M21-47 FUNCTION 1. 0. 1
20505601 VOIDF 02103000 011
20505700 L10M21-48 FUNCTION 1. 0. 1
20505701 VOIDF 02103000 011
20505800 L10M21-49 FUNCTION 1. 0. 1
20505801 VOIDF 02103000 011
20505900 L10M21-50 FUNCTION 1. 0. 1
20505901 VOIDF 02103000 011
20506000 L10M21-51 FUNCTION 1. 0. 1
20506001 VOIDF 02103000 011
20506100 L10M21-52 FUNCTION 1. 0. 1
20506101 VOIDF 02103000 011
20506200 L10M21-53 FUNCTION 1. 0. 1
20506201 VOIDF 02103000 011
20506300 L10M21-54 FUNCTION 1. 0. 1
20506301 VOIDF 02103000 011
20506400 L10M21-55 FUNCTION 1. 0. 1
20506401 VOIDF 02103000 011
20506500 L10M21-56 FUNCTION 1. 0. 1
20506501 VOIDF 02103000 011
20506600 L10M21-57 FUNCTION 1. 0. 1
20506601 VOIDF 02103000 011
20506700 L10M21-58 FUNCTION 1. 0. 1
20506701 VOIDF 02103000 011
20506800 L10M21-59 FUNCTION 1. 0. 1
20506801 VOIDF 02103000 011
20506900 L10M21-60 FUNCTION 1. 0. 1
20506901 VOIDF 02103000 011
20507000 L10M21-61 FUNCTION 1. 0. 1
20507001 VOIDF 02103000 011
20507100 L10M21-62 FUNCTION 1. 0. 1
20507101 VOIDF 02103000 011
20507200 L10M21-63 FUNCTION 1. 0. 1
20507201 VOIDF 02103000 011
20507300 L10M21-64 FUNCTION 1. 0. 1
20507301 VOIDF 02103000 011
20507400 L10M21-65 FUNCTION 1. 0. 1
20507401 VOIDF 02103000 011
20507500 L10M21-66 FUNCTION 1. 0. 1
20507501 VOIDF 02103000 011
20507600 L10M21-67 FUNCTION 1. 0. 1
20507601 VOIDF 02103000 011
20507700 L10M21-68 FUNCTION 1. 0. 1
20507701 VOIDF 02103000 011
20507800 L10M21-69 FUNCTION 1. 0. 1
20507801 VOIDF 02103000 011
20507900 L10M21-70 FUNCTION 1. 0. 1
20507901 VOIDF 02103000 011
20508000 L10M21-71 FUNCTION 1. 0. 1
20508001 VOIDF 02103000 011
20508100 L10M21-72 FUNCTION 1. 0. 1
20508101 VOIDF 02103000 011
20508200 L10M21-73 FUNCTION 1. 0. 1
20508201 VOIDF 02103000 011
20508300 L10M21-74 FUNCTION 1. 0. 1
20508301 VOIDF 02103000 011
20508400 L10M21-75 FUNCTION 1. 0. 1
20508401 VOIDF 02103000 011
20508500 L10M21-76 FUNCTION 1. 0. 1
20508501 VOIDF 02103000 011
20508600 L10M21-77 FUNCTION 1. 0. 1
20508601 VOIDF 02103000 011
20508700 L10M21-78 FUNCTION 1. 0. 1
20508701 VOIDF 02103000 011
20508800 L10M21-79 FUNCTION 1. 0. 1
20508801 VOIDF 02103000 011
20508900 L10M21-80 FUNCTION 1. 0. 1
20508901 VOIDF 02103000 011
20509000 L10M21-81 FUNCTION 1. 0. 1
20509001 VOIDF 02103000 011
20509100 L10M21-82 FUNCTION 1. 0. 1
20509101 VOIDF 02103000 011
20509200 L10M21-83 FUNCTION 1. 0. 1
20509201 VOIDF 02103000 011
20509300 L10M21-84 FUNCTION 1. 0. 1
20509301 VOIDF 02103000 011
20509400 L10M21-85 FUNCTION 1. 0. 1
20509401 VOIDF 02103000 011
20509500 L10M21-86 FUNCTION 1. 0. 1
20509501 VOIDF 02103000 011
20509600 L10M21-87 FUNCTION 1. 0. 1
20509601 VOIDF 02103000 011
20509700 L10M21-88 FUNCTION 1. 0. 1
20509701 VOIDF 02103000 011
20509800 L10M21-89 FUNCTION 1. 0. 1
20509801 VOIDF 02103000 011
20509900 L10M21-90 FUNCTION 1. 0. 1
20509901 VOIDF 02103000 011
20510000 L10M21-91 FUNCTION 1. 0. 1
20510001 VOIDF 02103000 011
20510100 L10M21-92 FUNCTION 1. 0. 1
20510101 VOIDF 02103000 011
20510200 L10M21-93 FUNCTION 1. 0. 1
20510201 VOIDF 02103000 011
20510300 L10M21-94 FUNCTION 1. 0. 1
20510301 VOIDF 02103000 011
20510400 L10M21-95 FUNCTION 1. 0. 1
20510401 VOIDF 02103000 011
20510500 L10M21-96 FUNCTION 1. 0. 1
20510501 VOIDF 02103000 011
20510600 L10M21-97 FUNCTION 1. 0. 1
20510601 VOIDF 02103000 011
20510700 L10M21-98 FUNCTION 1. 0. 1
20510701 VOIDF 02103000 011
20510800 L10M21-99 FUNCTION 1. 0. 1
20510801 VOIDF 02103000 011
20510900 L10M21-100 FUNCTION 1. 0. 1
20510901 VOIDF 02103000 011

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20501200 L10M21-3 FUNCTION 1. 0. 1
20501201 VOIDF 02103000 011
20504100 L10EVOC SUM 1. 0. 1
20504101 1.115 0.300 VOIDF 027010000
20504102 0.020 VOIDF 071000100
20504103 0.020 VOIDF 071070100
20504104 0.020 VOIDF 071040100
20504105 0.020 VOIDF 071050100
20504106 0.020 VOIDF 071040100
20504107 .146 VOIDF 071040100
20504108 1.2 CNTRLVAR 011
20504109 1.2 CNTRLVAR 011
20504110 0.404 VOIDF 071010100
* LIQUID LEVEL IN UPPER PLENUM AND STEAM PIPE
HEIGHT OF LIQUID - FCT OF LIQUID VOID
20702100 NORMAREA 0VOL21-1
20702101 0. 0. 0.100 0.022 0.336 0.000
20702102 0.654 0.230 0.075 0.369 1.0 0.525
20702103 0. 0. 0.100 0.022 0.336 0.000
20702104 0.654 0.230 0.075 0.369 1.0 0.525
20502100 L10M21-2 FUNCTION 1. 0. 1
20502101 VOIDF 057010000 021
20504200 L10EVAP SUM 1. 0. 1
20504201 0. 0.170 VOIDF 051010300
20504202 1.0 CNTRLVAR 021
20504203 0.952 VOIDF 057020300
* LIQUID LEVEL IN CORE
20504300 L10LCORE SUM 0.360 0. 1
20504301 0. 1. VOIDF 004010000
20504302 1. VOIDF 004020000
20504303 1. VOIDF 004030000
20504304 1. VOIDF 004040000
20504305 1. VOIDF 004050000
20504306 1. VOIDF 004060000
20504307 1. VOIDF 004070000
20504308 1. VOIDF 004080000
20504309 1. VOIDF 004090000
20504310 1. VOIDF 004100000
* LIQUID LEVEL IN LOWER PLENUM
20504400 L10LEVP SUM 1. 0. 1
20504401 0. 0.150 VOIDF 330100000
20504402 0.325 VOIDF 330100000
20504403 0.271 VOIDF 330100000
* *ROD CLADDING TEMP SAVE UP
20506100 CLADTEMP1 MULT 1. 0. 1
20506101 HTTEMP 401000103 *ROD CLADDING INNER TEMP VOL1
20506200 CLADTEMP2 MULT 1. 0. 1
20506201 HTTEMP 402000103 *ROD CLADDING INNER TEMP VOL2
20506300 CLADTEMP3 MULT 1. 0. 1
20506301 HTTEMP 403000103 *ROD CLADDING INNER TEMP VOL3
20506400 CLADTEMP4 MULT 1. 0. 1
20506401 HTTEMP 404000103 *ROD CLADDING INNER TEMP VOL4
20506500 CLADTEMP5 MULT 1. 0. 1
20506501 HTTEMP 405000103 *ROD CLADDING INNER TEMP VOL5
20506600 CLADTEMP6 MULT 1. 0. 1
20506601 HTTEMP 406000103 *ROD CLADDING INNER TEMP VOL6
20506700 CLADTEMP7 MULT 1. 0. 1
20506701 HTTEMP 407000103 *ROD CLADDING INNER TEMP VOL7
20506800 CLADTEMP8 MULT 1. 0. 1
20506801 HTTEMP 408000103 *ROD CLADDING INNER TEMP VOL8
20506900 CLADTEMP9 MULT 1. 0. 1
20506901 HTTEMP 409000103 *ROD CLADDING INNER TEMP VOL9
20507000 CLADTEMP10 MULT 1. 0. 1
20507001 HTTEMP 410000106 *ROD CLADDING MIDDLE TEMP VOL10
* HEAT TRANSFER COEFF (HEAT RATE/(SURFACE TEMP-FLUID TEMP))

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20508100 HICDEF1 SLM 1. 0. 1
 20508101 0. 1. HMFIC 401000101
 20508200 HICDEF2 SLM 1. 0. 1
 20508201 0. 1. HMFIC 402000101
 20508300 HICDEF3 SLM 1. 0. 1
 20508301 0. 1. HMFIC 403000101
 20508400 HICDEF4 SLM 1. 0. 1
 20508401 0. 1. HMFIC 404000101
 20508500 HICDEF5 SLM 1. 0. 1
 20508501 0. 1. HMFIC 405000101
 20508600 HICDEF6 SLM 1. 0. 1
 20508601 0. 1. HMFIC 406000101
 20508700 HICDEF7 SLM 1. 0. 1
 20508701 0. 1. HMFIC 407000101
 20508800 HICDEF8 SLM 1. 0. 1
 20508801 0. 1. HMFIC 408000101
 20508900 HICDEF9 SLM 1. 0. 1
 20508901 0. 1. HMFIC 409000101
 20509000 HICDEF10 SLM 1. 0. 1
 20509001 0. 1. HMFIC 410000101
 0 110010 LEVEL CONTROL SYSTEM FOR DC (STEADY STATE ONLY)
 20500000 LEVCTRLV TMDPVL
 2050101 1. 1. 0. 0. 0. 0. 00
 2050200 2. 7. 0. 0.
 2050301 0. 1. HMFIC 410000101
 4050000 LEVCTRLV TMDPVL
 4050101 20500000 071000000 0.3
 4050200 1 0 CTRLVAR 048
 4050301 -1. -1. 0. 0.
 4050302 1. 1. 0. 0.
 20504000 LEVCTR SLM 1. 0. 0
 20504001 0.412 -1. CTRLVAR 041
 20504900 SLEV MULT 25. 0. 0 3 -3. 3.
 20504901 CTRLVAR 28
 20504902 CTRLVAR 1
 0 SPRAY-FEED TEMPERATURE REGULATION
 0 DEL-1-(DT/DT0)*1/5.15DUSS*(W/J404
 0 DT/DT0)=.00218 KC/J
 0 DUSS-UC306-WF305-1.32 MJ/KG
 20502800 OTSPRAY INTEGRAL -68.8 434.18 0 2 437.18 456.18
 20502801 WFLOWJ 406000000
 0 STEAM RELIEF MASS LOSS SAVE UP
 20502900 SRELLOSS INTEGRAL 1. 0. 1
 20502901 WFLOWJ 404000000
 2060000 RELIEF TMDPVL
 2060101 0.00630 1. 0. 0. 90. 1. 0. 0. 00 *STEADY STATE
 2060200 2
 2060201 0. 8970000. 1.0 *REGULATED STEADY STATE
 4080000 DOMECTRL VALVE *STEADY STATE CARD
 4080101 013010000 306000000 0. 0. 1000 *STEADY STATE
 4080201 1 0. 0. 0. *STEADY STATE CARD
 4080300 TMDPVL
 4080301 601

20505000 STR-HILOSS SLM 1. 0. 1
 20505001 0. 17800 HTRMR 310000100
 20505002 26856 HTRMR 320000100
 20505003 27476 HTRMR 330000100
 20505004 14848 HTRMR 340000100
 20505005 17398 HTRMR 350000100
 20505006 28930 HTRMR 360000100
 20505007 21943 HTRMR 370000100
 20505008 9.48378 HTRMR 380000100
 20505009 40000 HTRMR 390000100
 20505010 63460 HTRMR 400000100
 20505011 88641 HTRMR 410000100
 20505012 23721 HTRMR 420000100
 20505013 42180 HTRMR 430000100
 20505014 34363 HTRMR 440000100
 20505015 34363 HTRMR 450000100
 20505016 34363 HTRMR 460000100
 20505017 28234 HTRMR 470000100
 20505018 28234 HTRMR 480000100
 20505019 28234 HTRMR 490000100
 20505020 28234 HTRMR 500000100
 20505100 STR-HILOSS SLM 1. 0. 0
 20505101 0. 28234 HTRMR 510000100
 20505102 28234 HTRMR 520000100
 20505103 24653 HTRMR 530000100
 20505104 12705 HTRMR 540000100
 20505105 25898 HTRMR 550000100
 20505106 66634 HTRMR 560000100
 20505107 36632 HTRMR 570000100
 20505108 83500 HTRMR 580000100
 20505109 67139 HTRMR 590000100
 20505110 43072 HTRMR 600000100
 20505111 40766 HTRMR 610000100
 20505112 41621 HTRMR 620000100
 20505113 28888 HTRMR 630000100
 20505114 80000 HTRMR 640000100
 20505115 -27351 HTRMR 650000100
 20505116 -81458 HTRMR 660000100
 20505117 -43102 HTRMR 670000100
 20505118 -78599 HTRMR 680000100
 20505119 30000 HTRMR 690000100
 20505120 31046 HTRMR 700000100
 20505200 STR-HILOSS SLM 1. 0. 0
 20505201 0. 18383 HTRMR 840000100
 20505202 26013 HTRMR 850000100
 20505203 24198 HTRMR 860000100
 20505204 42969 HTRMR 870000100
 20505205 27382 HTRMR 880000100
 20505206 26224 HTRMR 890000100
 20505207 85500 HTRMR 900000100
 20505300 TOTAL SLM 1. 0. 0
 20505301 0. 1. CTRLVAR 50
 20505302 1. CTRLVAR 51
 20505303 1. CTRLVAR 52
 20505400 STR-HIINT INTEGRAL 1. 0. 0
 20505401 CTRLVAR 50
 20505500 BREAK-LOSS INTEGRAL 1. 0. 0
 20505501 WFLOWJ 152000000
 20505600 BOX-HILOSS SLM 1. 0. 0
 20505601 0. 150 HTRMR 400000100

20605601 .150 HTRMR 400000100
 20605602 .150 HTRMR 400000300
 20605603 .150 HTRMR 400000400
 20605604 .150 HTRMR 400000500
 20605605 .150 HTRMR 400000600
 20605606 .150 HTRMR 400000700
 20605607 .150 HTRMR 400000800
 20605608 .150 HTRMR 400000900
 20605609 .150 HTRMR 400001000
 20605610 0
 20605700 COR-POW FUNCTION 1. 0. 0
 20605701 TIME 0 DO1
 20605800 BYPASS-POW FUNCTION 1. 0. 0
 20605801 TIME 0 DO2
 20605900 TOT-POW SLM 1. 0. 0
 20605901 0. 1. CTRLVAR 57
 20605902 1. CTRLVAR 58
 20606000 BREAK-LOSS INTEGRAL 1. 0. 0
 20606001 WFLOWJ 152000000
 ***** INITIAL VALUES
 0310200 3 7067230. 842.44
 0320200 3 7065410. 842.32
 0330200 3 7063160. 842.19
 0310200 2 6997000. 0.8727
 0130200 2 6970000. 1.0
 0730200 3 7007370. 843.27
 0740200 3 7011380. 843.21
 0420200 3 7016950. 838.00
 0910200 3 7008660. 843.05
 0920200 3 7008730. 839.67
 0940200 3 7011350. 842.90
 0950200 3 7074150. 842.55
 0960200 3 7072960. 400.
 0970200 3 7071130. 842.10
 0980200 3 7065110. 400.
 2070200 3 7072020. 843.10
 2071000 3 7061580. 842.77
 0041201 3 7032080. 846.70 0. 0. 0. 1
 0041202 3 7035560. 0.007669 0. 0. 0. 2
 0041203 2 7022150. 0.019922 0. 0. 0. 3
 0041204 2 7019260. 0.038597 0. 0. 0. 4
 0041205 2 7015670. 0.040237 0. 0. 0. 5
 0041206 2 7011610. 0.081132 0. 0. 0. 6
 0041207 2 7007200. 0.099700 0. 0. 0. 7
 0041208 2 7002430. 0.12384 0. 0. 0. 8
 0041209 2 6996460. 0.15144 0. 0. 0. 9
 0041210 2 6992510. 0.18148 0. 0. 0. 10
 0521201 2 6990640. 0.074352 0. 0. 0. 1
 0521202 2 6971140. 0.17403 0. 0. 0. 2
 0711201 2 6970990. 0.85075 0. 0. 0. 1
 0721201 2 6970500. 0.77374 0. 0. 0. 1
 0721202 2 6969990. 0.72654 0. 0. 0. 2
 0711201 2 6971470 0.23091 0. 0. 0. 1
 0711202 2 6970990. 0.07366 0. 0. 0. 2
 0711203 2 6975540. 0 0. 0. 0. 3
 0711204 2 6977140. 843.84 0. 0. 0. 4
 0711205 2 6980000. 843.40 0. 0. 0. 5
 0711206 2 7055300. 842.87 0. 0. 0. 6
 0641201 3 7016790. 845.55 0. 0. 0. 1

```

0441202 3 7006390 533 00 0. 0 0 3
0441203 3 6934760 556 50 0. 0. 0 3
0901201 3 7065140 541 50 0. 0. 0 3
0
0 JUNCTION INITIAL VALUES
0041300 0
0041301 1.263 1.454 0. 1 1.400 1.655 0. 3
0041302 1.700 2.029 0. 3 2.140 2.645 0. 4
0041303 2.647 3.263 0. 6 3.114 4.004 0. 6
0041304 3.645 4.657 0. 7 4.650 5.441 0. 6
0041305 4.710 5.886 0. 0
0571300 1
0571301 6.180 1.002 0. 1
0131300 1
0131301 -3.64 .10 0. 1
0211300 1
0211301 0.62 0. 0. 3
0311300 1
0311301 11.43 0. 0. 7
0741300 1
0741301 4.74 0. 0. 4
0441300 1
0441301 0.67 0. 0. 7
0901300 1
0901301 1.63 0 0. 1
0

```

Transient input, Case A

```

0 INPUT FOR RELAPS/AM2
0 FIN-11 CASILOPINE BREAK (RESTART (TEST NO 00411
0 300 B SPLIT BREAK (FILE FIN6A1)
0
0000100 RESTART TRANSIT
0000101 BEM
0000102 405
0000103 10. 20.
0000201 23. 1.0E-6 .0425 00001 16 1000 1000
0
0
0*****
0
0 TRIPS
0
0000501 TIME 0 GE NULL 0 0. 0 STEADY STATE
0
0 END

```

Steady state input, Case B

* INPUT FOR RELAPS/AM2
 * FIN-11 CUILLOTIME BREAK RESTART (TEST NO. 80411)
 * 700 & SPLIT BREAK (FILE F16G85)
 * CASE B, RESTART FROM CASE A STEADY STATE
 *

8000100 RESTART STDY-ST
 8000101 9LM
 8000102 405
 8000103 10.
 8000104 10. 30.
 8000105 10. 1.0E-8 .0475 80001 0 400 400

0111201 -4.468 1.118 0 1
 (END)

*
 * TRIPS
 8000501 TIME 0 CE MAX 0 80. 1 *STEADY STATE
 *

* VOL11 AND VOL12 MADE 4.0 TIMES HIGHER FOR MORE TRASS
 *

0110000 VOL11 ANMPLUS
 0110001 1
 0110101 0.0 1
 0110201 2.2222 1
 0110301 0.00070 1
 0110401 90. 1
 0110501 0. 0. 1
 0111001 00 1

0120000 VOL12 PIPE
 0120001 2
 0120101 0.0 2
 0120201 10.10 1 .034 2
 0120301 0.03700 1 0.01410 2
 0120401 90. 2
 0120501 0. 0. 2
 0121001 00 1 01 2
 0121101 1000 1

1870000 JUM11-21 SMCJLJM
 1870101 011000000 011000000 0.0 0.0 0.0 1000
 1870201 1 0.468 -1.118 0.

1880000 JUM12-11 SMCJLJM
 1880101 012000000 011010000 0. 0. 0. 1000
 1880201 1 0.468 -1.118 0.

4050000 LEVCIRJLM THOPJLM
 4050101 301000000 011000000 0.2
 4050201 1 0 CTRIVLAR 040
 4050301 -1. -1. .05 0.
 4050401 1. 1. -.05 0.

* ASSUMED QUALITY FOR MTOT-310 RG
 0111201 2 0070990. 0.15000 0. 0. 0. 1
 0111201 2 0070300. 0.40000 0. 0. 0. 1
 0111201 2 0049990. 0.35000 0. 0. 0. 2
 *
 0111300 1

Steady state input, Case C

```

* INPUT FOR DELAYS/MOOD
* FIN-11 CUILLOTIME BREAK RESTART (TEST NO 30611)
* 300 N SPILL BREAK (FILL SUBJECT)
* CASE C, RESTART FROM CASE 0 STEADY STATE
*
0000100 RESTART 310Y-3T
0000101 BLM
0000102 000
0000103 10. 70.
0000104 10. 1.0E-6 .0418 00001 16 1000 1000
*
*
* TRIPS
*
0000101 TIME 0 GE MALL 0 FS. L =STEADY STATE
*
*
0101000 PUMP1 PUMP
0101101 0. 0.750 0.01010 0. 16.4 0.703 0
0101102 0.7030000 0.00277 0.77 0.37 0000
0101103 0.7400000 0.000908 .0 .0 0170
0101104 3 7073070. 843.31
0101101 1 4.74 0. 0.
0101102 1 4.74 0. 0.
0101103 0 0 -1 0 0 0
0101104 303.00 0.0240 0.0303 50. 01.7 1. 1000.
0101105 0. 0. 0. 0.
* NIA MÅNÖRGA PUMPKURVOR. DATA KOMMER FRÅN ASEA-ATOMS DOBLIN-MER.
* TORQUE KURVORNA SÄKRAV BETYDELSE I DETTA FALL OCH HAR DÄRFÖR INTE
* KONTROLLERATS. KÄLLAN FÖR EN DEL DATA ÄR OKÄND.
0111100 1 1
0111101 0.00,1.101 0.27,1.100 0.47,1.100
0111102 0.84,1.130 1.00,1.000
0111200 2 1
0111201 0.00,0.04 0.00,0.07 0.10,0.00
0111202 0.30,0.01 0.10,0.04 0.00,0.00 1.00,1.00
0111300 1 2
0111301 0.0,-0.160 0.41,-0.10 0.01,-0.00 0.70,0.40
0111302 1.00,1.00
0111400 2 2
0111401 0.0,-1.16 0.1,0.00 0.00,0.30 1.00,1.00
0111500 1 3
0111501 -1.00,2.00 -0.00,1.01 -0.00,1.02 -0.00,1.00
0111502 0.00,1.10
0111600 1 4
0111601 -1.00,2.00 -0.70,1.03 -0.00,1.00 -0.30,0.00
0111602 0.00,0.72
0111700 2 3
0111701 -1.00,2.31 -0.00,2.70 -0.00,2.20 -0.00,1.00
0111702 -0.37,1.49 -0.22,1.10 -0.10,0.00 0.00,0.00
0111800 2 4
0111801 -1.00,2.31 -0.70,2.70 -0.00,2.37 -0.41,2.04
0111802 -0.21,1.70 0.00,1.00
* TWO PHASE MULTIPLIER TABLES
0130000 0
0130001 0.0,0.0 0.1,0.0 0.10,0.00 0.24,0.0 0.3,0.00 0.4,0.00
0130002 0.0,0.07 0.0,0.0 0.0,0.0 0.00,0.0 1.0,0.0
0131000 0
0131001 0.0,0.0 0.1,0.0 0.10,0.00 0.24,0.0 0.3,0.00 0.4,0.00
0131002 0.0,0.07 0.0,0.0 0.0,0.0 0.00,0.0 1.0,0.0

```

```

* TWO PHASE DIFFERENCE FOR PUMP HEAD (SEMISCALED)
0141000 1 1
0141001 0.0,0.0 0.1,0.00 0.2,1.00 0.0,1.00 0.7,1.01 0.0,0.0 1.0,0.1
0141002 1 2
0141001 0.0,0.0 0.1,-0.04 0.2,0.0 0.3,0.1 0.4,0.21 0.0,0.07
0141002 0.0,0.00 1.0,1.0
0141300 1 3
0141301 -1.0,-1.10 -0.0,-1.20 -0.0,-1.37 -0.7,-2.35 -0.0,-2.70
0141302 -0.0,-2.01 -0.4,-2.07 -0.2,-1.00 -0.1,-0.0 0.0,0.0
0141400 1 4
0141401 -1.0,-1.10 -0.0,-0.70 -0.0,-0.0 -0.7,-0.31 -0.0,-0.17
0141402 -0.0,-0.00 -0.20,0.0 -0.2,0.00 -0.1,0.00 0.0,0.11
* TWO PHASE DIFFERENCE FOR PUMP TORQUE (1- SINGLE PHASE, WHICH MEANS
* THAT FULLY DEGRADED TORQUE IS ZERO)
0141900 2 1
0141901 0.00,0.04 0.00,0.07 0.10,0.00
0141902 0.30,0.07 0.00,0.00 0.00,0.00 1.00,1.00
0151000 2 2
0151001 0.0,-1.16 0.0,0.00 0.00,0.30 1.00,1.00
0151100 2 3
0151101 -1.00,2.31 -0.00,2.70 -0.00,2.20 -0.00,1.00
0151102 -0.37,1.49 -0.22,1.10 -0.10,0.00 0.00,0.00
0151200 2 4
0151201 -1.00,2.31 -0.70,2.70 -0.00,2.37 -0.41,2.04
0151202 -0.21,1.70 0.00,1.00
* PUMP REGULATOR
0161000 0 CTRLVAR 000 1000. 1000.
0161101 0. 0.
*
*
0201000 PUMP2 PUMP
0201101 0. 0.700 0.00100 0. 72.0 0.770 0
0201102 0.7000000 0.0010 0.31 0.31 0000
0201103 0.7500000 0.000310 .0 .0 0170
0201200 2 7077010. 843.31
0201201 1 1.03 0. 0.
0201202 1 1.03 0. 0.
0201301 0 0 -1 0 0 0
0201302 303.00 0.0010 0.0100 75. 13.2 1. 1000
0201303 0. 0. 0.
0211000 1 1
0211101 0.0 1.130 0.2 1.130 0.4 1.120
0211102 0.0 1.100 0.0 1.010 1.0 1.010
0211200 2 1
0211201 0.0 0.01 1.0 1.00
0211300 1 2
0211301 0.0 -0.000 0.2 -0.000 0.4 -0.100 0.0 -0.000
0211302 0.0 0.145 0.0 0.000 1.0 1.000
0211400 2 2
0211401 0.0 -0.47 0.2 -0.21 0.4 0.07
0211402 0.0 0.35 0.0 0.00 1.0 1.00
0211500 1 3
0211501 -1.00,2.00 -0.00,1.01 -0.00,1.02 -0.00,1.00
0211502 0.00,1.10
0211600 1 4
0211601 -1.00,2.00 -0.70,1.03 -0.00,1.00 -0.30,0.00
0211602 0.00,0.72
0211700 2 3
0211701 -1.00,2.31 -0.00,2.70 -0.00,2.20 -0.00,1.00
0211702 -0.37,1.49 -0.22,1.10 -0.10,0.00 0.00,0.00
0211800 2 4
0211801 -1.00,2.31 -0.70,2.70 -0.00,2.37 -0.41,2.04
0211802 -0.21,1.70 0.00,1.00
0230000 0
0230001 0.0,0.00 0.1,0.00 0.2,0.00 0.3,0.00 0.4,0.00 0.0,0.00

```

```

0230002 0.0,0.07 0.0,0.00 0.0,0.00 0.0,0.00 1.0,0.00
0231000 0
0231001 0.0,0.00 0.1,0.00 0.2,0.00 0.3,0.00 0.4,0.00 0.0,0.00
0231002 0.0,0.00 0.0,0.00 0.0,0.00 0.0,0.00 1.0,0.00
* PUMP REGULATOR
0261000 0 CTRLVAR 010 1000. 1000.
*
*
* END

```

Steady state input, Case D

INPUT FOR RELAPS/ACD
FILE= C:\RELAP\BREAM\RESTART\TEST NO. 30813
100 B SPLIN BREAK FILE #194051
CASE 0, RESTART FROM CASE 0 STEADY STATE

0000100 RESTART 3107-31
0000101 RUN
0000102 935
0000103 10.
0000104 10. 1.0E-6 .0618 00001 16 1000 1000

TRIPS
0000101 TIME 0 CE MALL 0 35. L STEADY STATE

0110000 VOL11 ANGLUS
0110001 1
0110101 0.0 0
0110201 0. 1 0.031132 3 0. 7
0110301 0.404 1 0.549 2 .0718 6 .0730 0
0110401 0.07189 1 0.04788 2 0.001175 6 0.007635 0
0110501 -90. 0
0110601 0. 0.3948 1 0. 0.2892 2 0. 0.1818 0 0. 0.1117 0
0110701 0. 0. 1 0.96 0.96 3 0. 0. 7
0110801 00 0
0110901 1000 7

0110000 VOL11 PIPE
0110001 10
0110101 0.0 16
0110201 -.49318 0 .40990 10
0110301 0.004573 0 0.007843 10
0110401 0. 6 -.90. 16
0110501 0. 0. 16
0110601 0.00 0.00 5 0.10 0.10 0 0.00 0.00 15
0110701 00 16
0110801 1000 15

0150000 VOL15 PIPE
0150001 3
0150101 0.0 3
0150201 0.0418 7
0150301 0.00168 3
0150401 14.3 2
0150501 .2081 2
0150601 0. 0. 2
0150701 0.00 0.00 1
0150801 00 2
0150901 1000 1

0160000 VOL16 PIPE
0160001 3
0160101 0.0 3
0160201 0.4017 3
0160301 0.007097 3
0160401 0. 2
0160501 0. 0. 3

0140001 0.00 0.00 3
0141001 00 3
0141101 1000 3

01130000 4 4 2 1 .133
01130100 0 7
01130101 0.005 1 0.018 2 0.01 3
01130201 3 3
01130301 .0 3
01130401 160. 4
01130501 21070000 010000 1 1 .0718 4
01130601 -13 0 3014 1 .0718 4
01130701 0 .0 .0 0 4
01130801 0 .0 .0 .0 4

01210000 2 4 2 1 .132
01210100 0 2
01210101 0.005 1 0.018 2 0.01 3
01210201 3 3
01210301 .0 3
01210401 160. 4
01210501 21070000 010000 1 1 .073 2
01210601 -13 0 3014 1 .073 2
01210701 0 .0 .0 .0 2
01210801 0 .0 .0 .0 2

01100000 16 3 2 1 .0146
01100100 0 1
01100101 2 .0707
01100201 3 2
01100301 .0 2
01100401 160. 3
01100501 71070000 010700 1 1 0.49335 0
01100601 71070000 010700 1 1 0.4099 16
01100601 -13 0 3014 1 0.49335 0
01100601 -13 0 3014 1 0.4099 16
01100701 0 .0 .0 .0 15
01100801 0 .0 .0 .0 15

01500000 2 3 2 1 .0146
01500100 0 1
01500101 2 .0701
01500201 3 2
01500301 .0 2
01500401 160. 3
01500501 95010000 010000 1 1 .0418 2
01500601 -13 0 3014 1 .0418 2
01500701 0 .0 .0 .0 2
01500801 0 .0 .0 .0 2

01600000 3 3 2 1 .0269
01600100 0 1
01600101 2 .0448
01600201 3 2
01600301 .0 2
01600401 160 0 3
01600501 96010000 010000 1 1 .4917 3
01600601 0 0 0 1 .4917 3
01600701 0 0. 0. 0. 3
01600801 0 0. 0. 0. 3

0111201 2 6902560. 0.24380 0. 0. 0. 1
0111202 2 6903950. 0.02758 0. 0. 0. 2
0111203 2 6904340. 0.0 0. 0. 0. 0

0111204	2	6907740.	0.03 97	0.	0.	0.	0.	0.
0111201	2	6906110.	0.43 94	0.	0.	0.	0.	0.
0111202	2	6904000.	0.43 90	0.	0.	0.	0.	0.
0111203	2	6905900	0.43 87	0.	0.	0.	0.	0.
0111204	2	6908050.	0.43 84	0.	0.	0.	0.	0.
0111205	2	6904950.	0.43 82	0.	0.	0.	0.	0.
0111206	2	7001030.	0.43 79	0.	0.	0.	0.	0.
0111207	2	7001160.	0.43 77	0.	0.	0.	0.	0.
0111208	2	7013160.	0.43 74	0.	0.	0.	0.	0.
0111209	2	7055410.	0.43 73	0.	0.	0.	0.	0.
0111201	2	1073350.	400.	0.	0.	0.	0.	0.
0111300	1							
0111301	0 62	0.	0. 7					
0111300	1							
0111301	11.42	0.	0. 16					
0151300	1							
0151301	1.53	0.	0. 1					
0161300	1							
0161301	1	0.	0. 2					

APPENDIX B

Data comparison plots

PLOT NO.	IDENT.	QUANTITY	(EXPERIMENT) (CALCULATIONS)
B. 1	----	-----	
	RN1?	FLUID DENSITY, CORE BOTTOM (RHO 0401)	CASE ?
B. 2	D 4 PD4?	DIFF. PRESSURE, CORE INLET RESTRICTION (DPT 4)	- EXPERIMENT DIFF PRESSURE, CORE INLET RESTRICTION (P 3301 - P 401) CASE ?
B. 3	X801 HP1? HL1?	ELECTRIC POWER, CORE - EXPERIMENT CORE HEATING POWER (CNTRLVAR 57)	CASE ? HEAT LOSS FROM PASSIVES (CNTRLVAR 53) CASE ?
B. 4	TC 1 NT1?	MEAN CLAD TEMP.. LEVEL 1 (T191 T206 T211 T246)	- EXPERIMENT MEAN CLAD TEMPERATURE, LEVEL 1 (NTTEMP 401000105) CASE ?
B. 5	TC 3 NT2?	MEAN CLAD TEMP.. LEVEL 3 (T108 T183 T243 T248)	- EXPERIMENT MEAN CLAD TEMPERATURE, LEVEL 3 (NTTEMP 403000105) CASE ?
B. 6	TC 5 NT3?	MEAN CLAD TEMP.. LEVEL 5 (T202 T227 T232 T237 T252)	- EXPERIMENT MEAN CLAD TEMPERATURE, LEVEL 5 (NTTEMP 404000105) CASE ?
B. 7	TC 7 NT4?	MEAN CLAD TEMP.. LEVEL 7 (T101 TO T271, 16 RODS)	- EXPERIMENT MEAN CLAD TEMPERATURE, LEVEL 5 (NTTEMP 405000105) CASE ?
B. 8	TC 9 NT5?	MEAN CLAD TEMP.. LEVEL 9 (T102 T137 T167 T172 T187 T197 T272)	- EXPERIMENT MEAN CLAD TEMPERATURE, LEVEL 9 (NTTEMP 406000105) CASE ?
B. 9	TC12 NT6?	MEAN CLAD TEMP.. LEVEL 12 (T118 T123 T128 T148 T223)	- EXPERIMENT MEAN CLAD TEMPERATURE, LEVEL 12 (NTTEMP 408000105) CASE ?
B.10	TC15 NT7?	MEAN CLAD TEMP.. LEVEL 15 (T175 T190 T275)	- EXPERIMENT MEAN CLAD TEMPERATURE, LEVEL 15 (NTTEMP 410000105) CASE ?
B.11	T 3 TF1?	FLUID TEMPERATURE, CORE INLET (TE 3)	- EXPERIMENT FLUID TEMPERATURE, CORE INLET (TEMPF 3301) CASE ?
B.12	T 14 TF2?	FLUID TEMPERATURE, CORE OUTLET (TE 14)	- EXPERIMENT FLUID TEMPERATURE, CORE OUTLET (TEMPF 5101) CASE ?
B.13	D CO PDC?	DIFF. PRESSURE, CORE (DPT 5 + DPT 6 + + DPT 12)	- EXPERIMENT DIFF PRESSURE, CORE (FROM P 401 - P 5101) CASE ?
B.14	----	-----	
	RN2?	FLUID DENSITY, VESSEL BOTTOM (RHO 3101)	CASE ?
B.15	D DC PDD?	DIFF. PRESSURE, DOWNCOMER (DPT 27 + + DPT 30)	- EXPERIMENT DIFF PRESSURE, DOWNCOMER (FROM P 7103 - P 7201) CASE ?
B.16	D LP PDL?	DIFF. PRESSURE, LOWER FLENUM (DPT 2 + DPT 3 - DPT 1)	- EXPERIMENT DIFF PRESSURE, LOWER FLENUM (FROM P 3101 - P 3301) CASE ?
B.17	D UP PDU?	DIFF. PRESSURE, UPPER FLENUM (DPT 13 + DPT 14)	- EXPERIMENT DIFF PRESSURE, UPPER FLENUM (FROM P 5101 - P 5201) CASE ?
B.18	D 56 PDS?	DIFF. PRESSURE, STEAM SEPARATOR ORIFICE (DPT 56)	- EXPERIMENT DIFF PRESSURE, STEAM SEPARATOR ORIFICE (P 5201 - P 5202) CASE ?
B.19	T 31 TF3?	FLUID TEMPERATURE, DOWN COMER BOTTOM (TE 31)	- EXPERIMENT FLUID TEMPERATURE, DOWNCOMER BOTTOM (TEMPF 7108) CASE ?

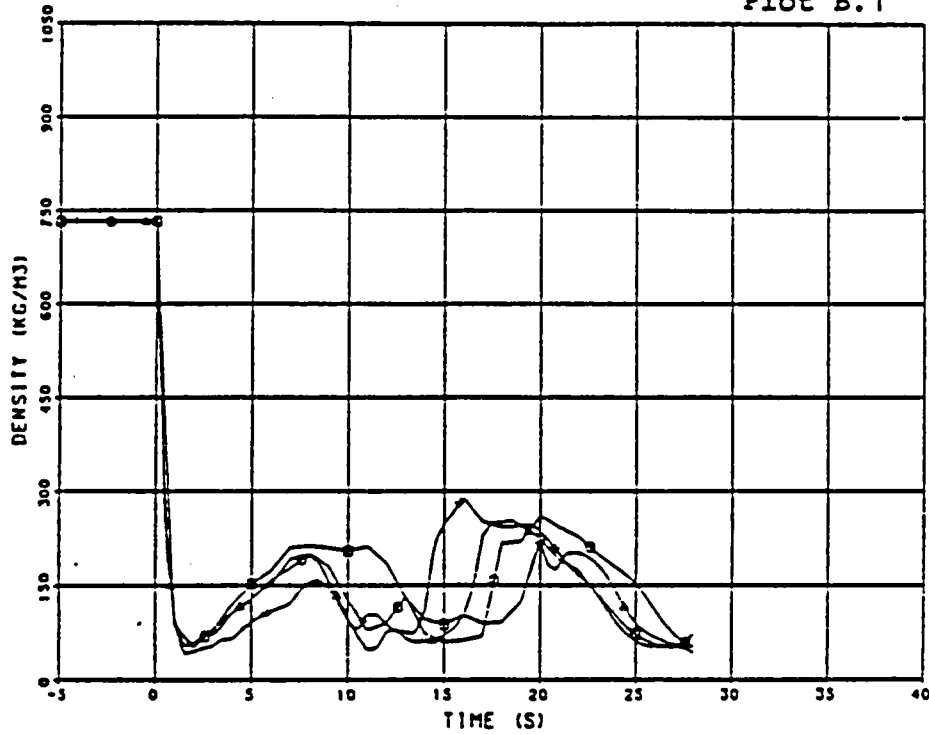
1986-10-28

PLCT NO.	IDENT.	QUANTITY	(EXPERIMENT) (CALCULATIONS)
B.20	T 15 TF4?	FLUID TEMPERATURE, UPPER PLENUM (TE 15) - EXPERIMENT FLUID TEMPERATURE, UPPER PLENUM (TEMPF 5201) CASE ?	
B.21	P 3 P 1?	PRESSURE, LOWER PLENUM (PT 3) - EXPERIMENT PRESSURE LOWER PLENUM (P 3101) CASE ?	
B.22	P 4 P 2?	PRESSURE, UPPER PLENUM (PT 4) - EXPERIMENT PRESSURE, UPPER PLENUM (P 5201) CASE ?	
B.23	X602 MF1?	MASS FLOW RATE, BYPASS - EXPERIMENT MASS FLOW RATE, BYPASS (MFLOWJ 117) CASE ?	
B.24	X603 MF2?	MASS FLOW RATE, I.L. PUMP - EXPERIMENT MASS FLOW RATE, I.L. PUMP (MFLOWJ 20102) CASE ?	
B.25	X604 MF3?	MASS FLOW RATE, B.L. PUMP - EXPERIMENT MASS FLOW RATE, B.L. PUMP (MFLOWJ 20202) CASE ?	
B.26	X610 MF4?	MASS FLOW RATE, B.L. VESSEL INLET (SPOOL PIECE K10) - EXPERIMENT MASS FLOW RATE, B.L. VESSEL INLET (MFLOWJ 9901) CASE ?	
B.27	---- MAT?	- - - - - TOTAL MASS, IN SYSTEM CASE ?	
B.28	X607 MF5?	MASS FLOW RATE, STEAM RELIEF - EXPERIMENT MASS FLOW RATE, STEAM RELIEF (MFLOWJ 404) CASE ?	
B.29	---- RM3?	- - - - - FLUID DENSITY, BREAK (RHO 9601) CASE ?	
B.30	X636 MF6?	MASS FLOW RATE, BREAK FROM T2 INVENTORY - EXPERIMENT MASS FLOW RATE, BREAK (MFLOWJ 152) CASE ?	
B.31	---- MF7?	- - - - - MASS FLOW RATE, BREAK (MFLOWJ 151) CASE ?	
B.32	X671 ML1?	MASS LOSS, BREAK FLOW RECIEVER T2 - EXPERIMENT BREAK TOTAL MASS LOSS (CNTRLVAR 55) CASE ?	
B.33	---- ML2?	- - - - - BREAK TOTAL MASS LOSS (CNTRLVAR 60) CASE ?	
B.34	T 34 TF5?	FLUID TEMPERATURE, BREAK INLET (TE 34) - EXPERIMENT FLUID TEMPERATURE, BREAK INLET (TEMPF 9601) CASE ?	
B.35	---- TSU?	- - - - - SUBCOOLING, BREAK INLET (TEMPG 9101 - TEMPF 9101) CASE ?	
B.36	P 6 P 3?	PRESSURE, BREAK INLET (PT 6) - EXPERIMENT PRESSURE, BREAK INLET (P 9601) CASE ?	
B.37	---- CPU?	- - - - - CPUTIME CASE ?	
B.38	---- MAE?	- - - - - MASS ERROR CASE ?	

↑>00 FLUID DENSITY. CORE BOTTOM (RHO 0401) CASE A
FLUID DENSITY. CORE BOTTOM (RHO 0401) CASE B
↓ FLUID DENSITY. CORE BOTTOM (RHO 0401) CASE C
FLUID DENSITY. CORE BOTTOM (RHO 0401) CASE D

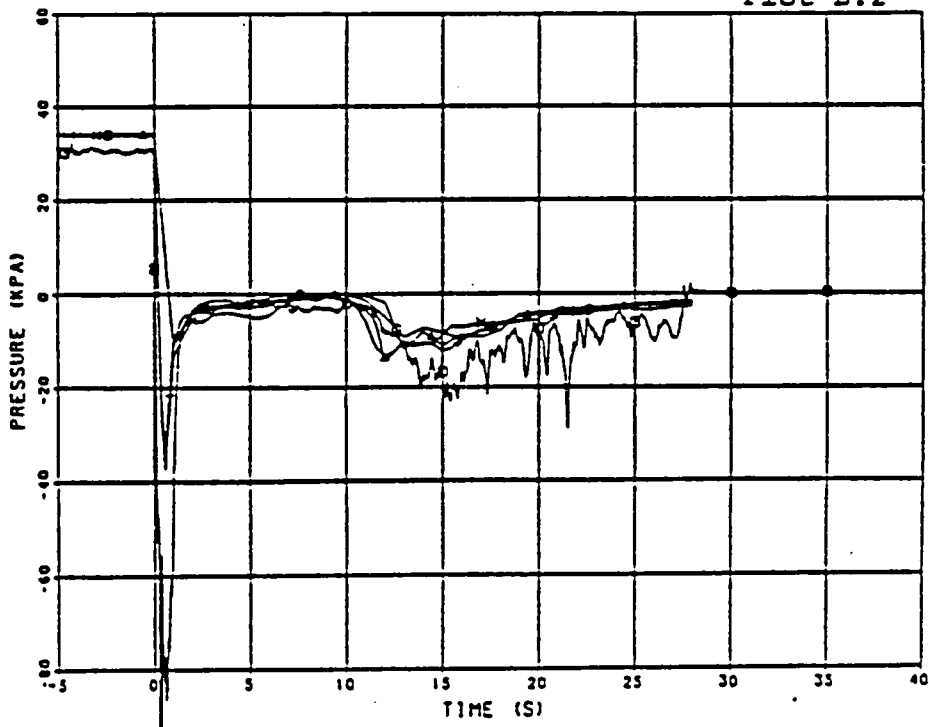
RELAP5/MOD2 CALCULATION FOR FIX-11. EXP 5061

Plot B.1



↑>00 DIFF. PRESSURE. CORE INLET RESTRICTION (OPT 4) - EXPERIMENT
DIFF. PRESSURE. CORE INLET RESTRICTION (P 3301 - P 401) CAS
↓ DIFF. PRESSURE. CORE INLET RESTRICTION (P 3301 - P 401) CAS
DIFF. PRESSURE. CORE INLET RESTRICTION (P 3301 - P 401) CAS
DIFF. PRESSURE. CORE INLET RESTRICTION (P 3301 - P 401) CAS

Plot B.2

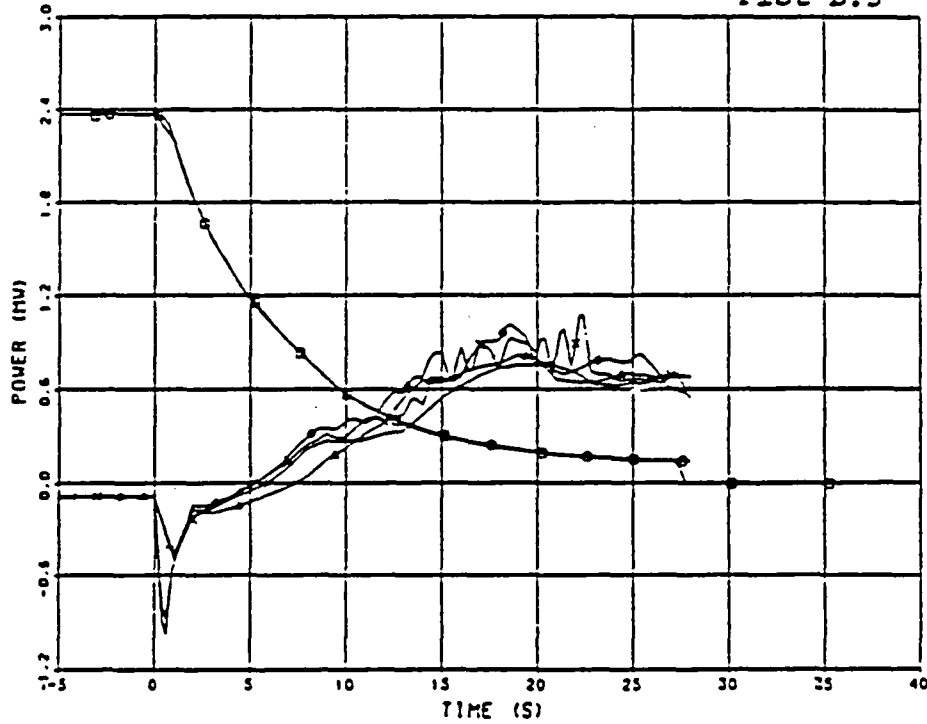


1986-10-28

RELAPS/MOD2 CALCULATION FOR FIX-II. EXP 5061

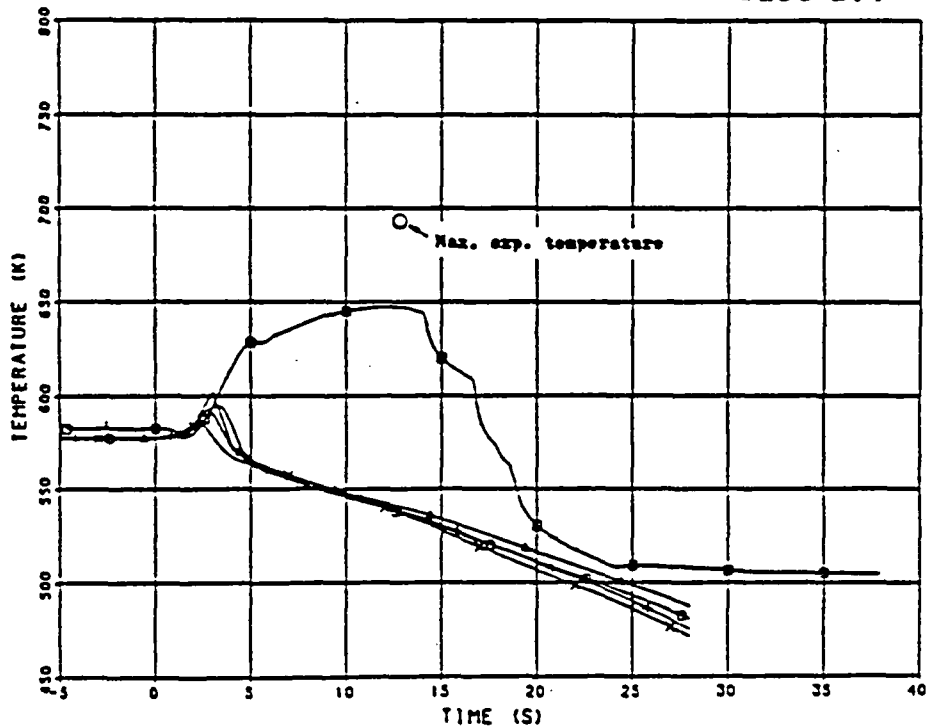
U ELECTRIC POWER, CORE - EXPERIMENT
 CORE HEATING POWER (CNTRLVAR 57) CASE A
 HEAT LOSS FROM PASSIVES (CNTRLVAR 53) CASE A
 HEAT LOSS FROM PASSIVES (CNTRLVAR 53) CASE B
 HEAT LOSS FROM PASSIVES (CNTRLVAR 53) CASE C
 HEAT LOSS FROM PASSIVES (CNTRLVAR 53) CASE D

Plot B.3



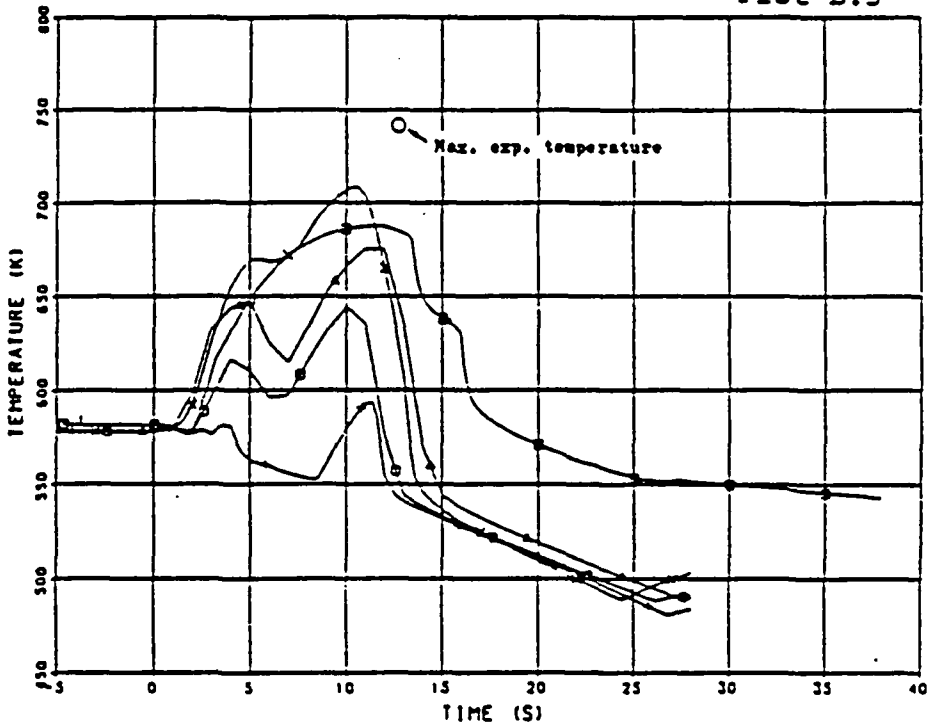
X 4000 NEAR CLAD TEMP., LEVEL 1 (T101 T206 T211 T246) - EXPERIMENT
 NEAR CLAD TEMPERATURE, LEVEL 1 (INTTEMP 401000103) CASE A
 NEAR CLAD TEMPERATURE, LEVEL 1 (INTTEMP 401000103) CASE B
 NEAR CLAD TEMPERATURE, LEVEL 1 (INTTEMP 401000103) CASE C
 NEAR CLAD TEMPERATURE, LEVEL 1 (INTTEMP 401000103) CASE D

Plot B.4



X+000 MEAN CLAD TEMP. LEVEL 3 (T108 T183 T243 T246) - EXPERIMENT
MEAN CLAD TEMPERATURE. LEVEL 3 INITTEMP 4030001031 CASE A
MEAN CLAD TEMPERATURE. LEVEL 3 INITTEMP 4030001031 CASE B
MEAN CLAD TEMPERATURE. LEVEL 3 INITTEMP 4030001031 CASE C
MEAN CLAD TEMPERATURE. LEVEL 3 INITTEMP 4030001031 CASE D

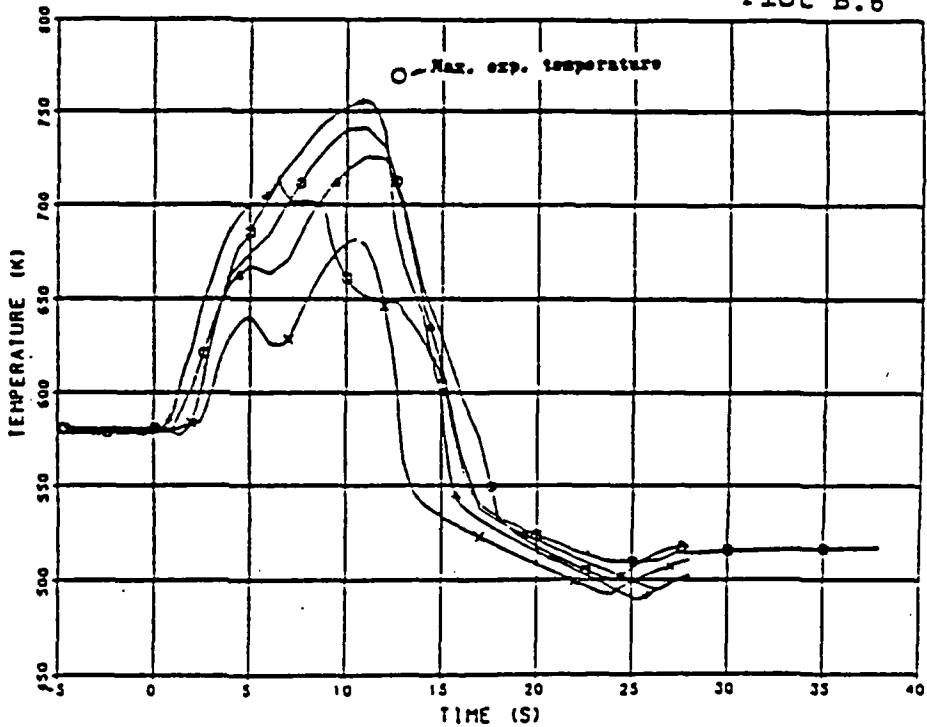
Plot B.5



RELAPS/MOD2 CALCULATION FOR FIX-11. EXP 5061

X+000 MEAN CLAD TEMP. LEVEL 3 (T202 T227 T232 T237 T232) - EXPER
MEAN CLAD TEMPERATURE. LEVEL 3 INITTEMP 4040001031 CASE A
MEAN CLAD TEMPERATURE. LEVEL 3 INITTEMP 4040001031 CASE B
MEAN CLAD TEMPERATURE. LEVEL 3 INITTEMP 4040001031 CASE C
MEAN CLAD TEMPERATURE. LEVEL 3 INITTEMP 4040001031 CASE D

Plot B.6



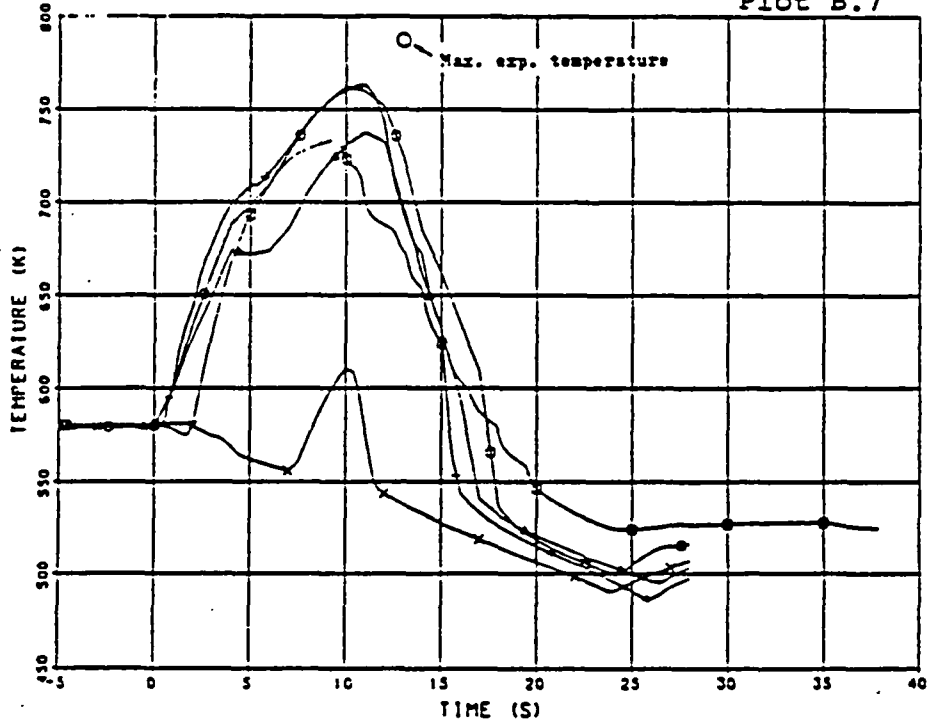
1986-10-28

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X 4 9 0 0 0  MEAN CLAD TEMPERATURE. LEVEL 7 (110) TO 127). 16 RODS) - EXPERIMENT
MEAN CLAD TEMPERATURE. LEVEL 7 (INITIAL 403000103) CASE A
MEAN CLAD TEMPERATURE. LEVEL 7 (INITIAL 403000103) CASE B
MEAN CLAD TEMPERATURE. LEVEL 7 (INITIAL 403000103) CASE C
MEAN CLAD TEMPERATURE. LEVEL 7 (INITIAL 403000103) CASE D

```

Plot B.7



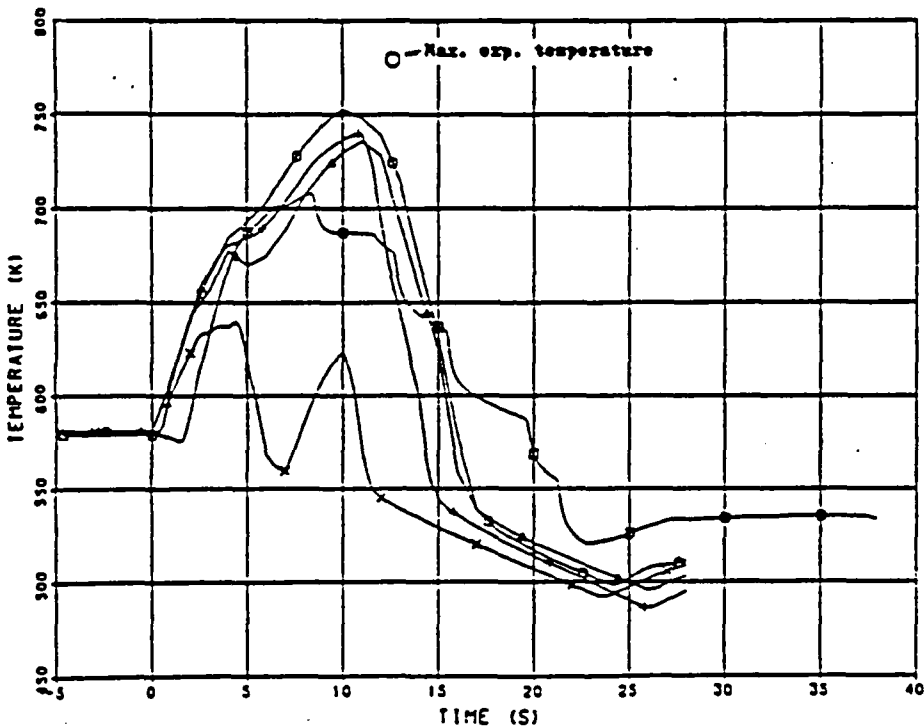
RELAP5/MOD2 CALCULATION FOR FIX-11. EXP 5061

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X 4 9 0 0 0  MEAN CLAD TEMPERATURE. LEVEL 9 (1102 1137 1167 1172 1187 1197 127
MEAN CLAD TEMPERATURE. LEVEL 9 (INITIAL 406000103) CASE A
MEAN CLAD TEMPERATURE. LEVEL 9 (INITIAL 406000103) CASE B
MEAN CLAD TEMPERATURE. LEVEL 9 (INITIAL 406000103) CASE C
MEAN CLAD TEMPERATURE. LEVEL 9 (INITIAL 406000103) CASE D

```

Plot B.8

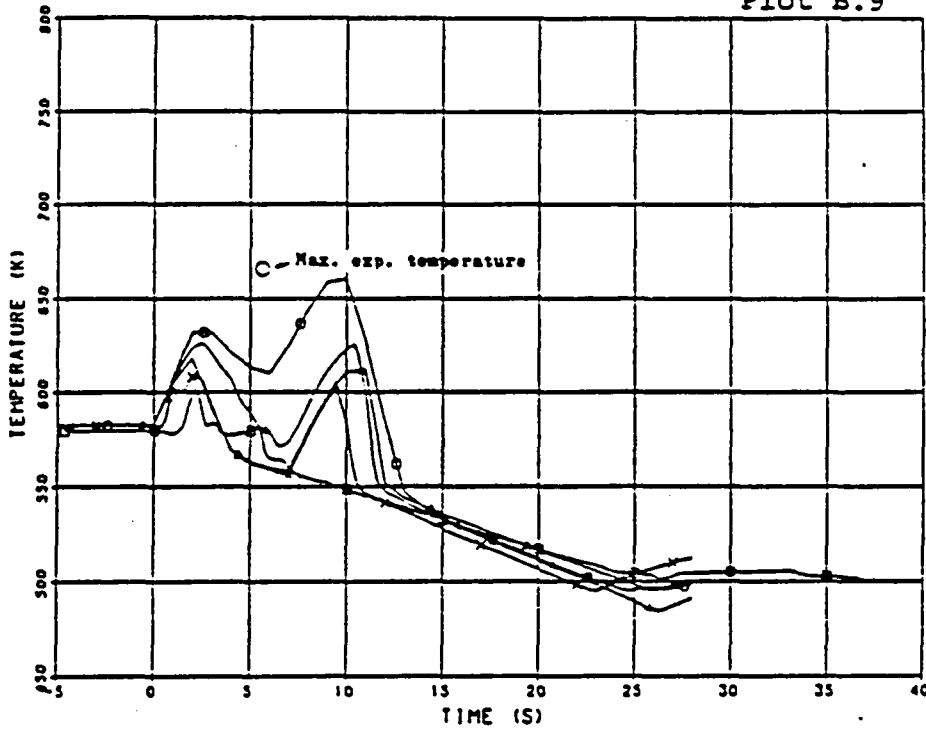


1986-10-28

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X+000 MEAN CLAD TEM. . LEVEL 12 (1118 1123 1128 1148 1223) - EXPE
MEAN CLAD TEMPERATURE. LEVEL 12 (INTEMP 407000103) CASE A
MEAN CLAD TEMPERATURE. LEVEL 12 (INTEMP 407000103) CASE B
MEAN CLAD TEMPERATURE. LEVEL 12 (INTEMP 407000103) CASE C
MEAN CLAD TEMPERATURE. LEVEL 12 (INTEMP 407000103) CASE D
    
```

Plot B.9

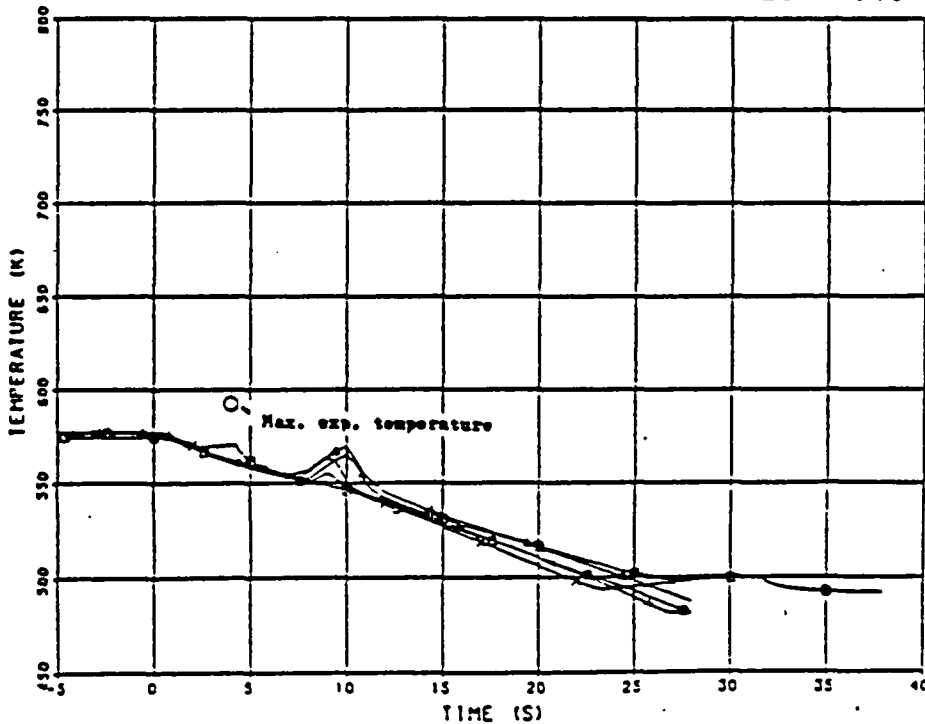


RELAPS/MOD2 CALCULATION FOR FIX-11. EXP 5061

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X+000 MEAN CLAD TEM. . LEVEL 13 (1175 1180 1273) - EXPERIMENT
MEAN CLAD TEMPERATURE. LEVEL 13 (INTEMP 410000103) CASE A
MEAN CLAD TEMPERATURE. LEVEL 13 (INTEMP 410000103) CASE B
MEAN CLAD TEMPERATURE. LEVEL 13 (INTEMP 410000103) CASE C
MEAN CLAD TEMPERATURE. LEVEL 13 (INTEMP 410000103) CASE D
    
```

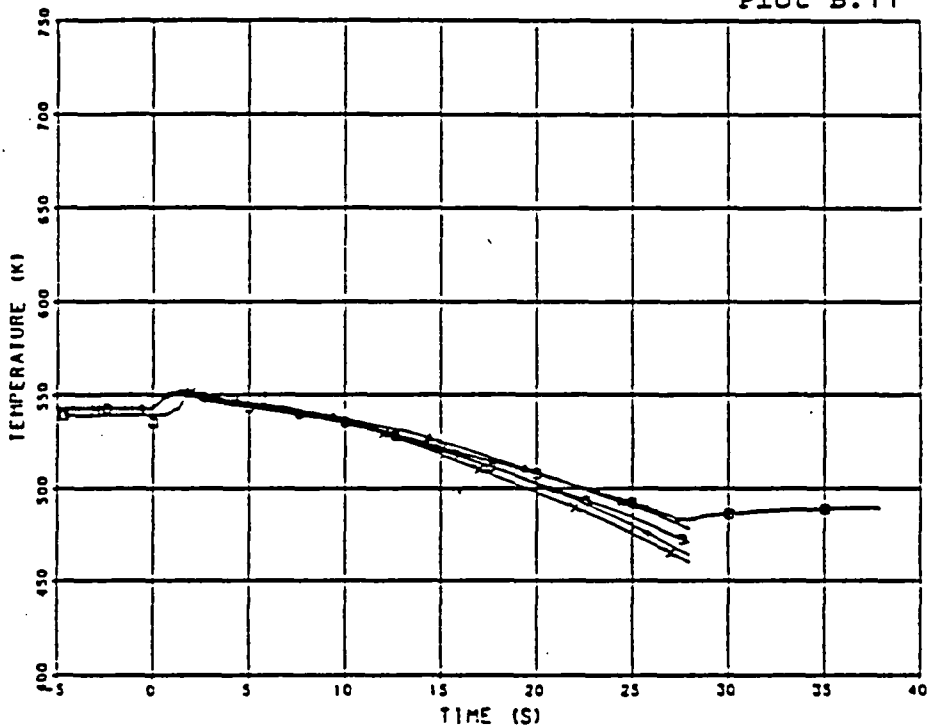
Plot B.10



RELAP5/MOD2 CALCULATION FOR FIX-11. EXP 5061

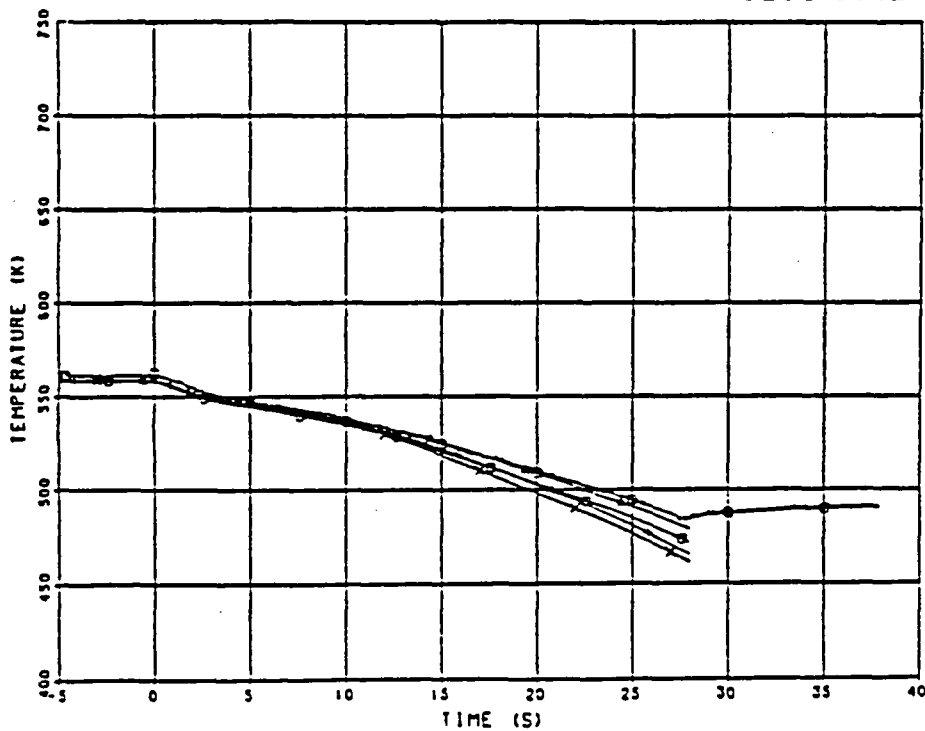
X > 0.0 FLUID TEMPERATURE. CORE INLET (ITE 3) - EXPERIMENT
 FLUID TEMPERATURE. CORE INLET (TEMPF 3301) CASE A
 FLUID TEMPERATURE. CORE INLET (TEMPF 3301) CASE B
 FLUID TEMPERATURE. CORE INLET (TEMPF 3301) CASE C
 FLUID TEMPERATURE. CORE INLET (TEMPF 3301) CASE D

Plot B.11



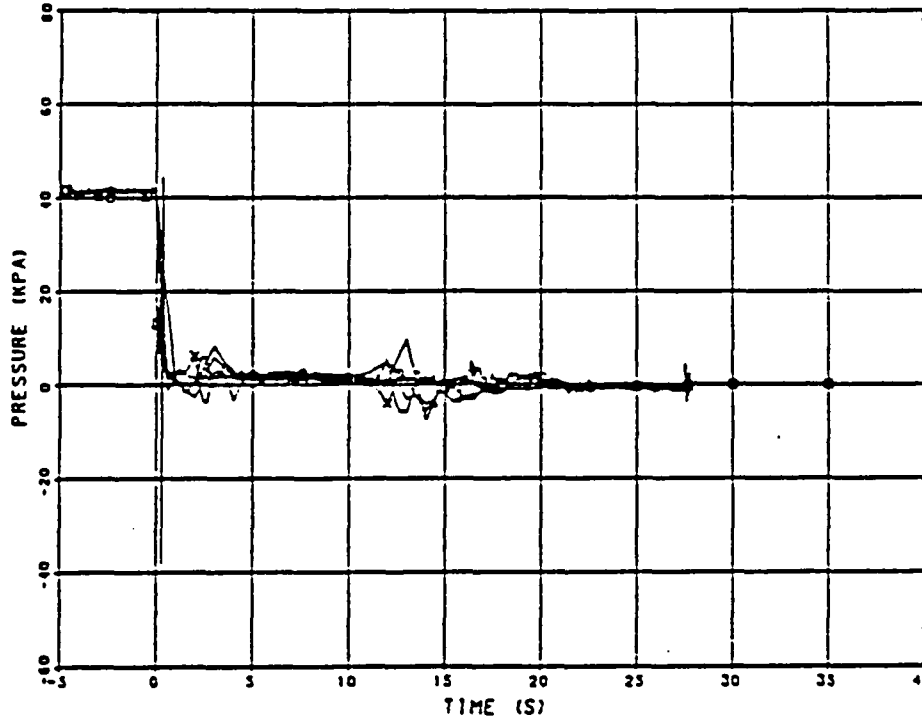
X > 0.0 FLUID TEMPERATURE. CORE OUTLET (ITE 14) - EXPERIMENT
 FLUID TEMPERATURE. CORE OUTLET (TEMPF 3101) CASE A
 FLUID TEMPERATURE. CORE OUTLET (TEMPF 3101) CASE B
 FLUID TEMPERATURE. CORE OUTLET (TEMPF 3101) CASE C
 FLUID TEMPERATURE. CORE OUTLET (TEMPF 3101) CASE D

Plot B.12



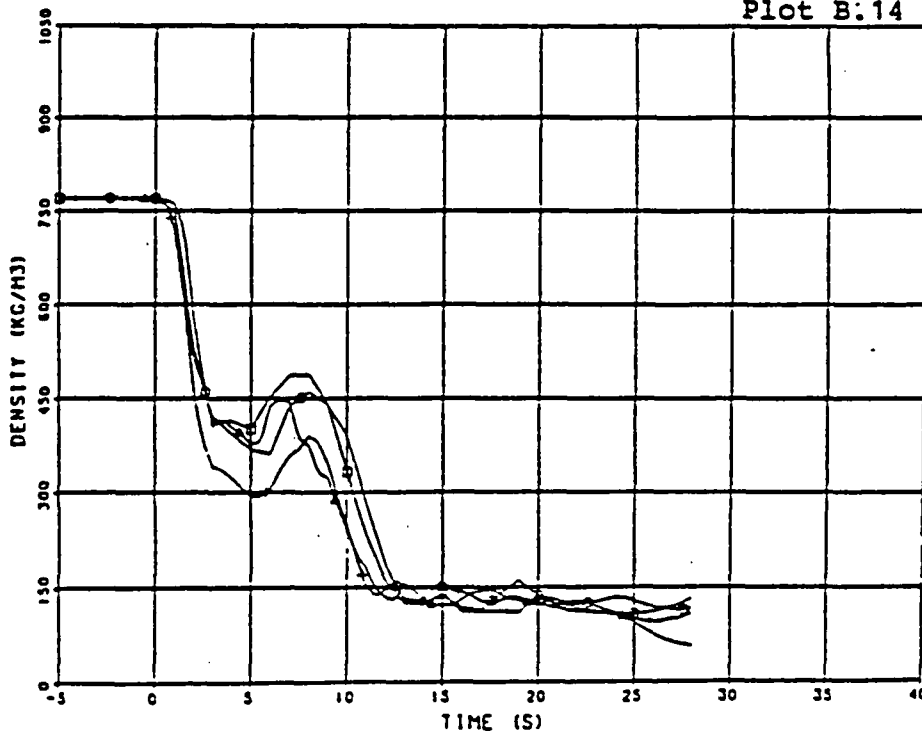
4900 DIFF PRESSURE. CORE (DPT 5 - DPT 6 - DPT 12) - EXPE
4900 DIFF PRESSURE. CORE (FROM P 401 - P 3101) CASE A
4900 DIFF PRESSURE. CORE (FROM P 401 - P 3101) CASE B
4900 DIFF PRESSURE. CORE (FROM P 401 - P 3101) CASE C
4900 DIFF PRESSURE. CORE (FROM P 401 - P 3101) CASE D

Plot B.13



4900 FLUID DENSITY. VESSEL BOTTOM (RNO 3101) CASE A
4900 FLUID DENSITY. VESSEL BOTTOM (RNO 3101) CASE B
4900 FLUID DENSITY. VESSEL BOTTOM (RNO 3101) CASE C
4900 FLUID DENSITY. VESSEL BOTTOM (RNO 3101) CASE D

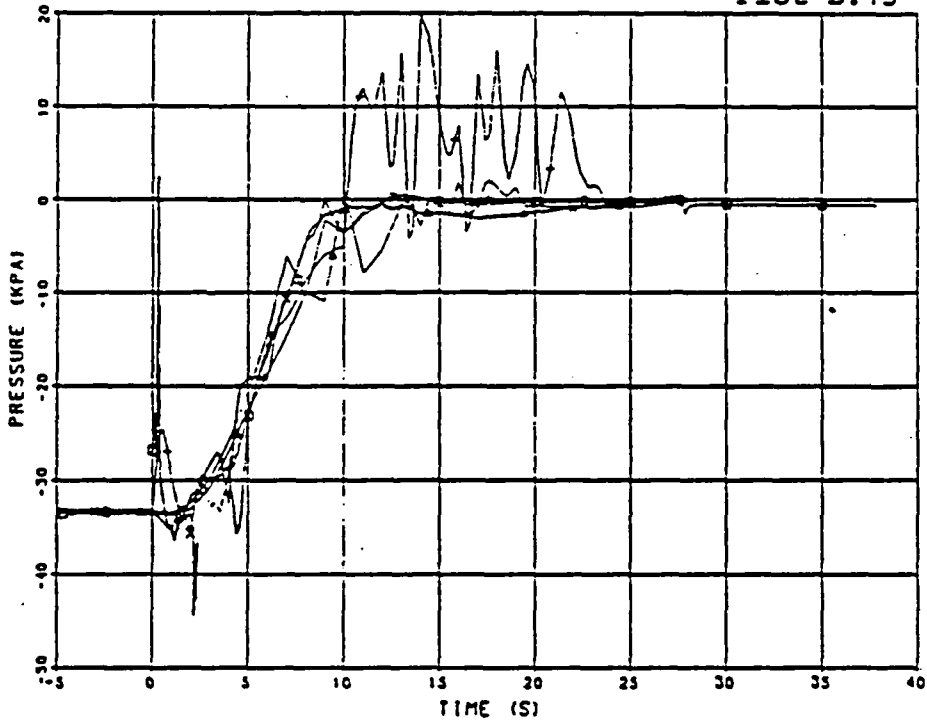
Plot B.14



RELAP5/MOD2 CALCULATION FOR FIX-11. EXP 5061

X + + + + +
DIFF. PRESSURE. DOWNCOMER (DP1 27 - DP1 30) - EXPERI
DIFF. PRESSURE. DOWNCOMER (FROM P 7103 - P 7201) CASE A
DIFF. PRESSURE. DOWNCOMER (FROM P 7103 - P 7201) CASE B
DIFF. PRESSURE. DOWNCOMER (FROM P 7103 - P 7201) CASE C
DIFF. PRESSURE. DOWNCOMER (FROM P 7103 - P 7201) CASE D

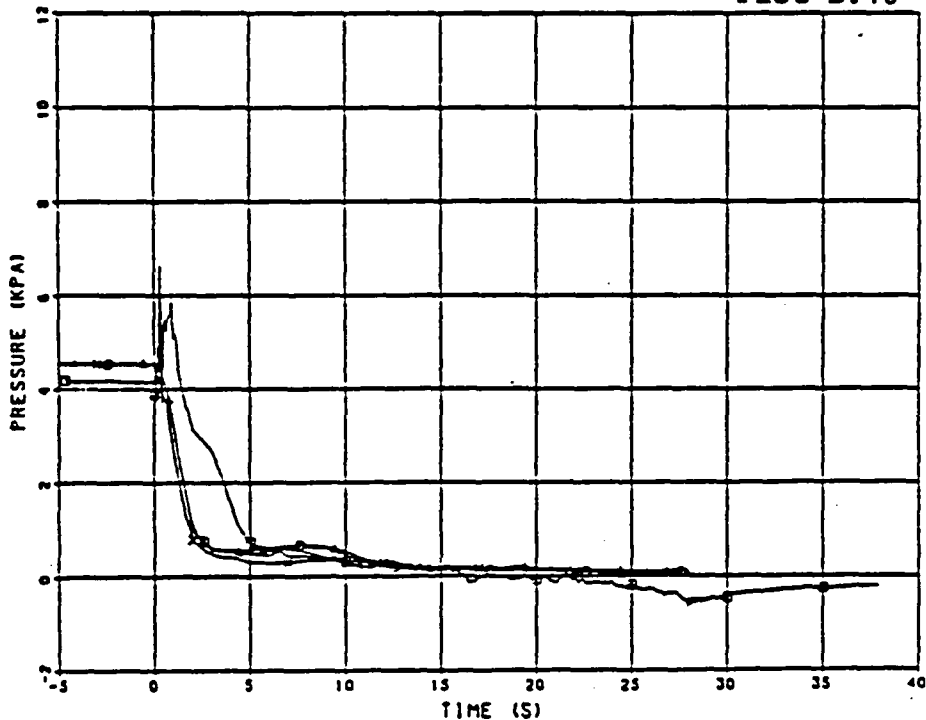
Plot B.15



RELAPS/MOD2 CALCULATION FOR FIX-11. EXP 5061

X + + + + +
DIFF. PRESSURE. LOWER PLENUM (DP1 2 - DP1 3 - DP1 11) - EXPERI
DIFF. PRESSURE. LOWER PLENUM (FROM P 3101 - P 3301) CASE A
DIFF. PRESSURE. LOWER PLENUM (FROM P 3101 - P 3301) CASE B
DIFF. PRESSURE. LOWER PLENUM (FROM P 3101 - P 3301) CASE C
DIFF. PRESSURE. LOWER PLENUM (FROM P 3101 - P 3301) CASE D

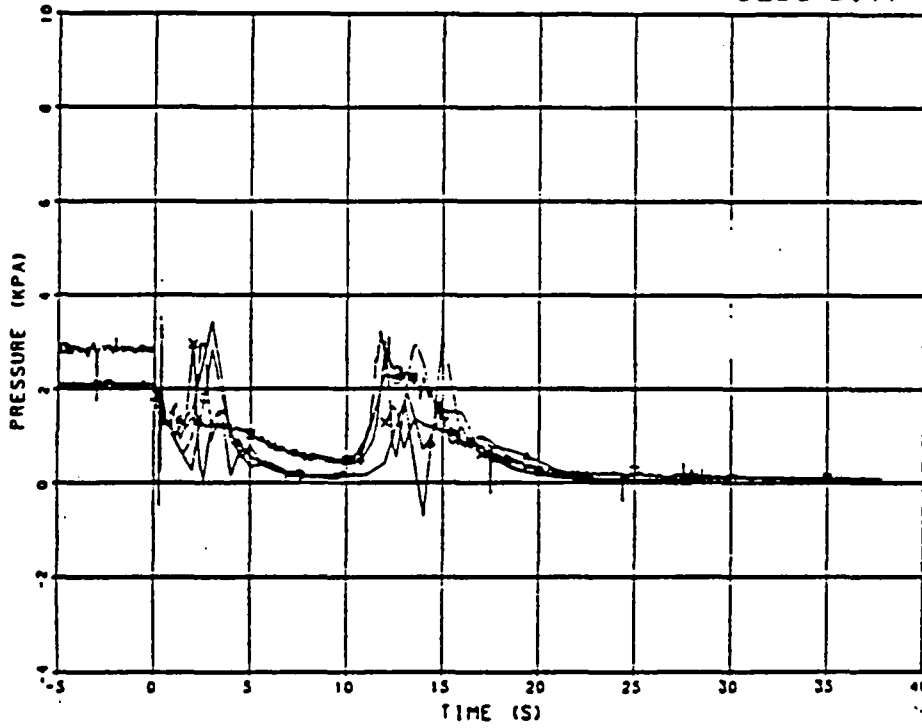
Plot B.16



1986-10-28

X+800 DIFF. PRESSURE. UPPER PLENUM (OPT 13 - OPT 14) - EXPERIMENT
DIFF. PRESSURE. UPPER PLENUM (FROM P 3101 - P 3201) CASE A
DIFF. PRESSURE. UPPER PLENUM (FROM P 3101 - P 3201) CASE B
DIFF. PRESSURE. UPPER PLENUM (FROM P 3101 - P 3201) CASE C
DIFF. PRESSURE. UPPER PLENUM (FROM P 3101 - P 3201) CASE D

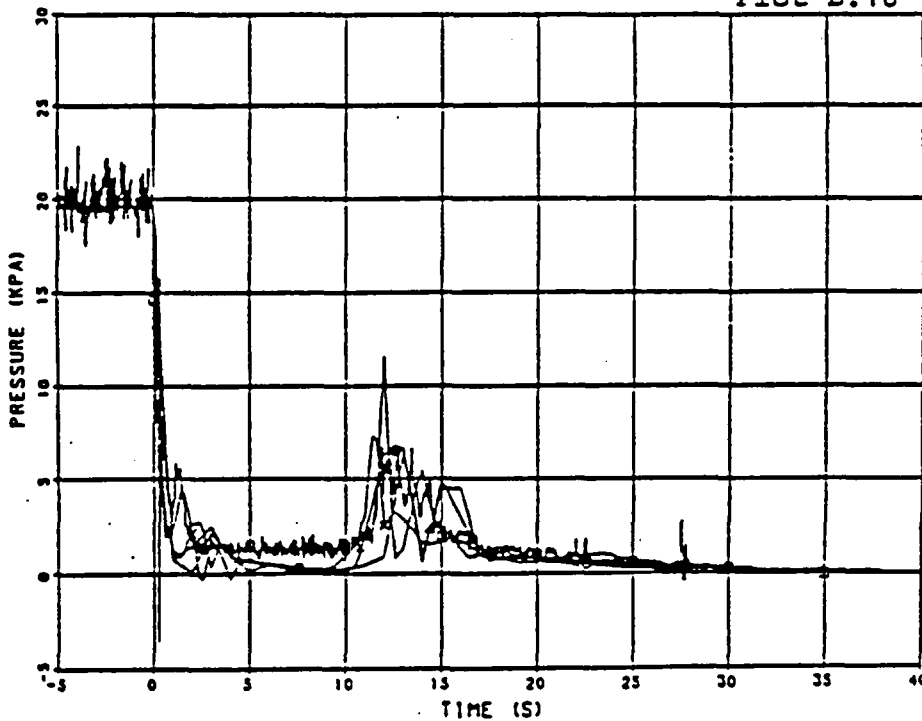
Plot B.17



RELAPS/MOD2 CALCULATION FOR FIX-11. EXP 5061

X+800 DIFF. PRESSURE. STEAM SEPARATOR ORIFICE (OPT 38) - EXPERIMENT
DIFF. PRESSURE. STEAM SEPARATOR ORIFICE (P 3201 - P 3202) C
DIFF. PRESSURE. STEAM SEPARATOR ORIFICE (P 3201 - P 3202) C
DIFF. PRESSURE. STEAM SEPARATOR ORIFICE (P 3201 - P 3202) C
DIFF. PRESSURE. STEAM SEPARATOR ORIFICE (P 3201 - P 3202) C

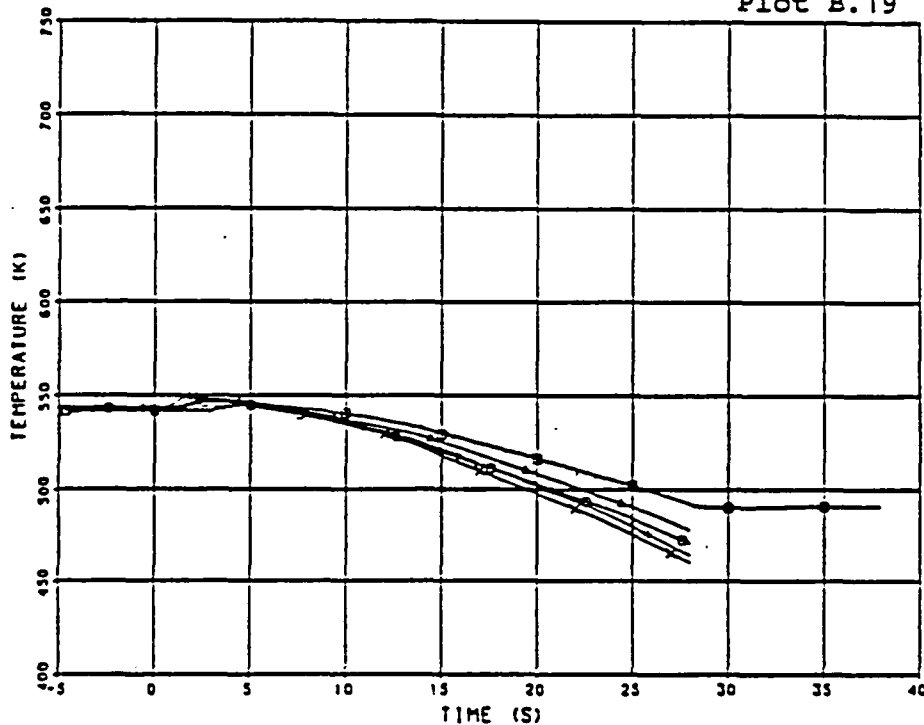
Plot B.18



RELAPS/MOD2 CALCULATION FOR FIX-11. EXP 5061

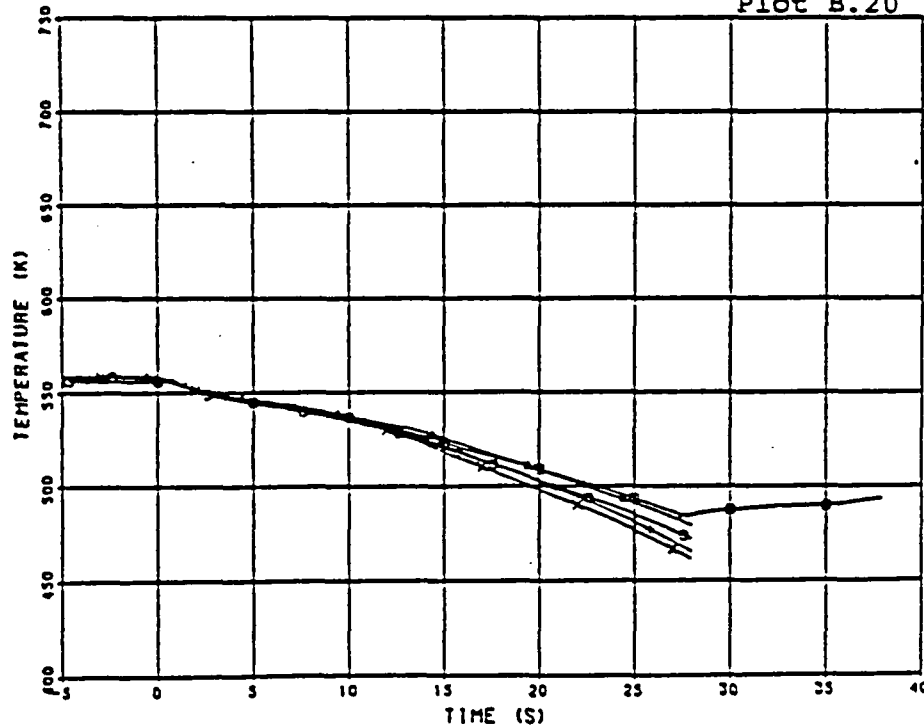
FLUID TEMPERATURE. DOWN COMER BOTTOM (ITE 31) - EXPERIMENT
FLUID TEMPERATURE. DOWNCOMER BOTTOM (TEMPF 7108) CASE A
FLUID TEMPERATURE. DOWNCOMER BOTTOM (TEMPF 7108) CASE B
FLUID TEMPERATURE. DOWNCOMER BOTTOM (TEMPF 7108) CASE C
FLUID TEMPERATURE. DOWNCOMER BOTTOM (TEMPF 7108) CASE D

Plot B.19



FLUID TEMPERATURE. UPPER PLENUM (ITE 13) - EXPERIMENT
FLUID TEMPERATURE. UPPER PLENUM (TEMPF 3201) CASE A
FLUID TEMPERATURE. UPPER PLENUM (TEMPF 3201) CASE B
FLUID TEMPERATURE. UPPER PLENUM (TEMPF 3201) CASE C
FLUID TEMPERATURE. UPPER PLENUM (TEMPF 3201) CASE D

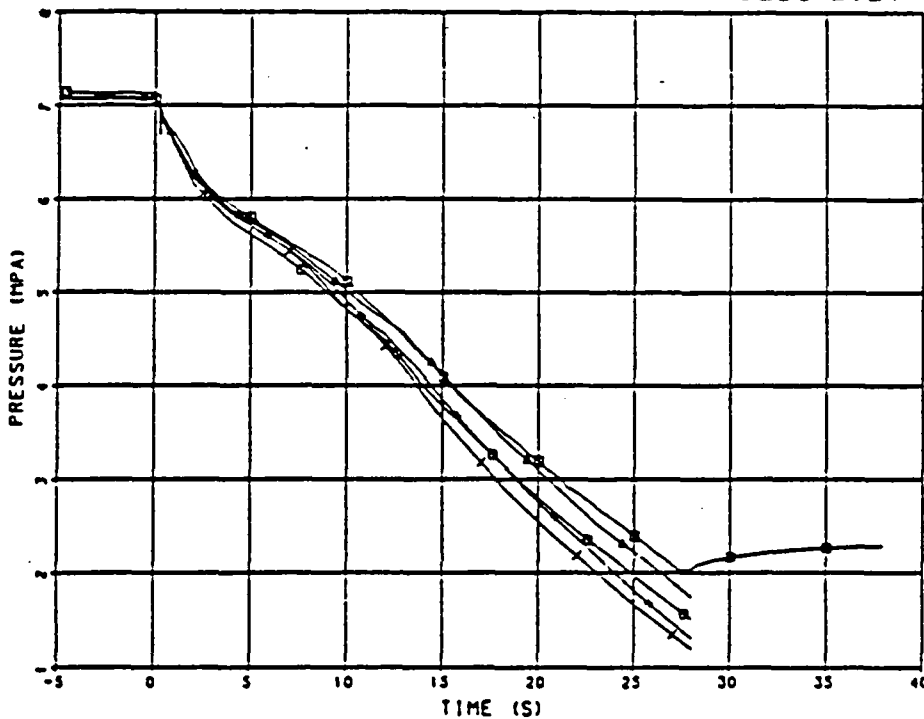
Plot B.20



RELAP5/MOD2 CALCULATION FOR FIX-11, EXP 5061

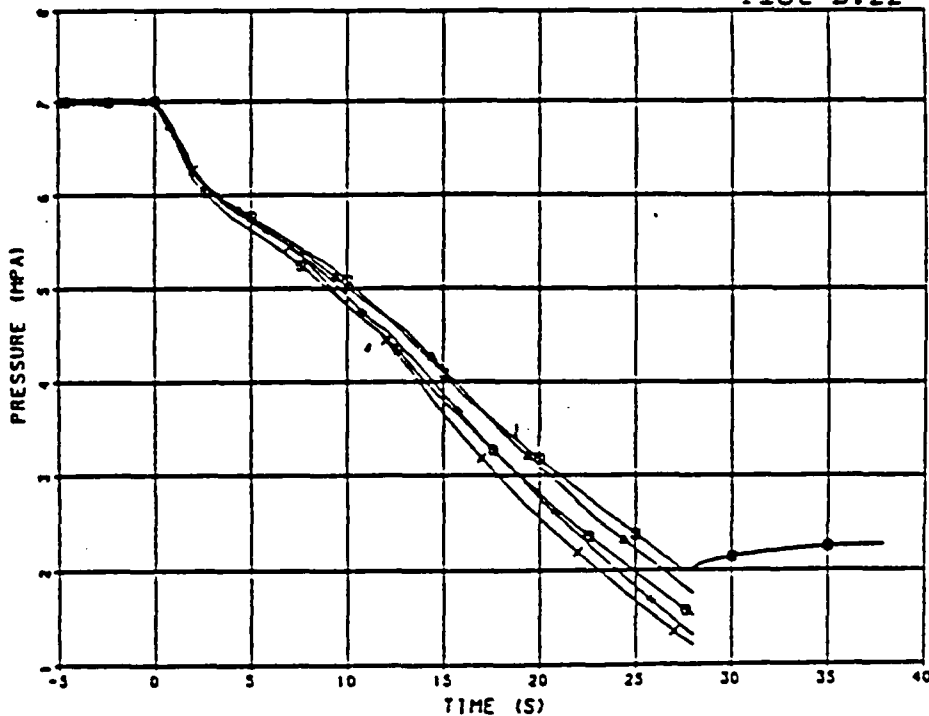
X+000 PRESSURE, LOWER PLENUM (P1 3) - EXPERIMENT
 X+000 PRESSURE, LOWER PLENUM (P 3101) CASE A
 X+000 PRESSURE, LOWER PLENUM (P 3101) CASE B
 X+000 PRESSURE, LOWER PLENUM (P 3101) CASE C
 X+000 PRESSURE, LOWER PLENUM (P 3101) CASE D

Plot B.21



X+000 PRESSURE, UPPER PLENUM (P1 4) - EXPERIMENT
 X+000 PRESSURE, UPPER PLENUM (P 5201) CASE A
 X+000 PRESSURE, UPPER PLENUM (P 5201) CASE B
 X+000 PRESSURE, UPPER PLENUM (P 5201) CASE C
 X+000 PRESSURE, UPPER PLENUM (P 5201) CASE D

Plot B.22

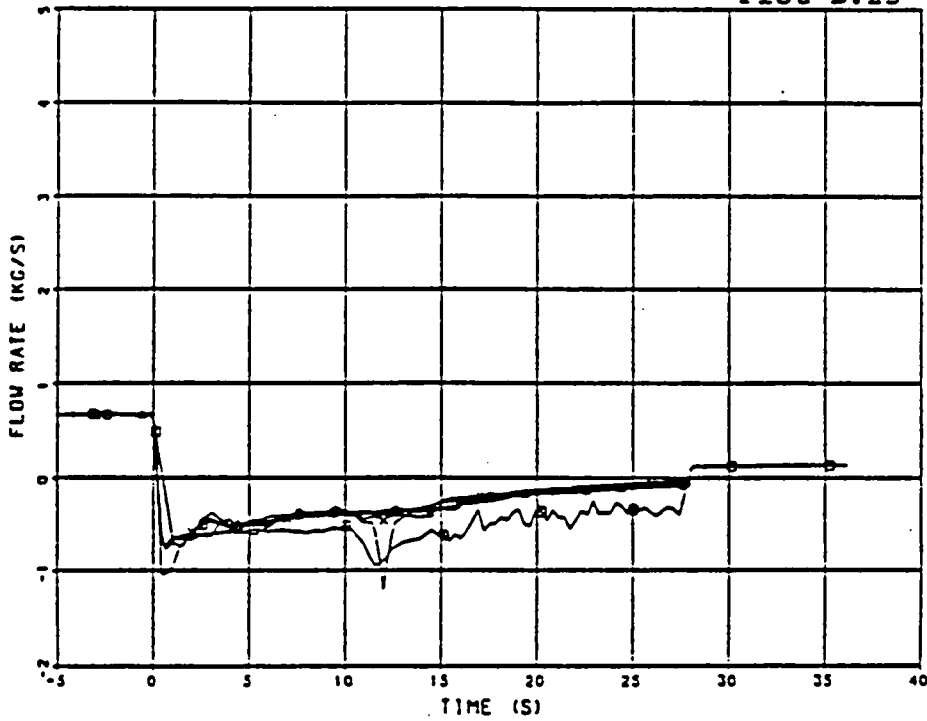


1986-10-28

RELAP5/MOD2 CALCULATION FOR FIX-11. EXP 5061

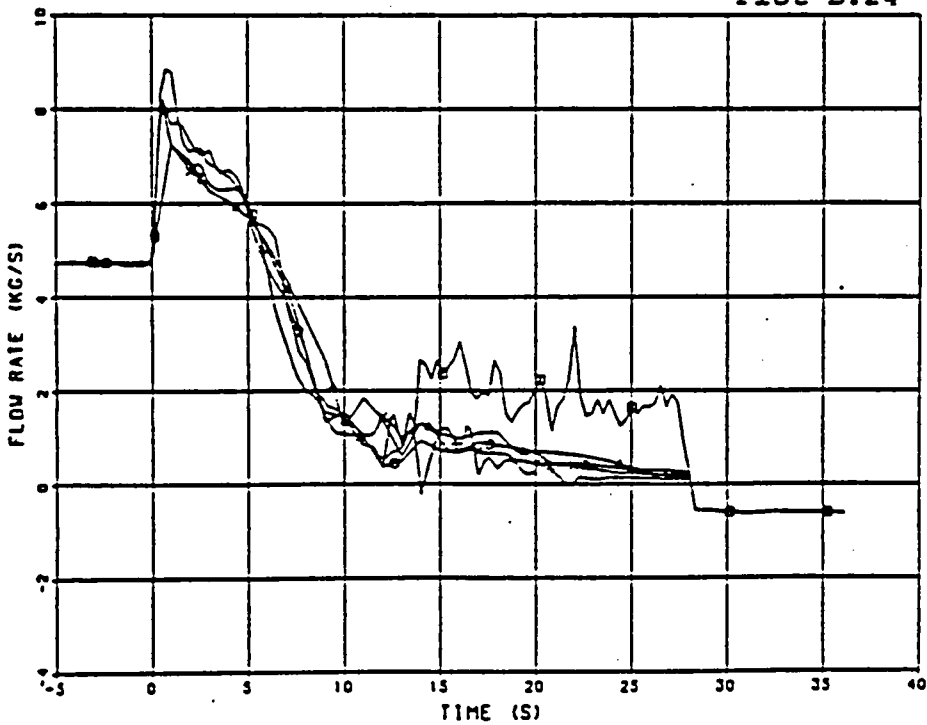
X 000 MASS FLOW RATE. BYPASS - EXPERIMENT
MASS FLOW RATE. BYPASS (FLOWJ 117) CASE A
MASS FLOW RATE. BYPASS (FLOWJ 117) CASE B
MASS FLOW RATE. BYPASS (FLOWJ 117) CASE C
MASS FLOW RATE. BYPASS (FLOWJ 117) CASE D

Plot B.23



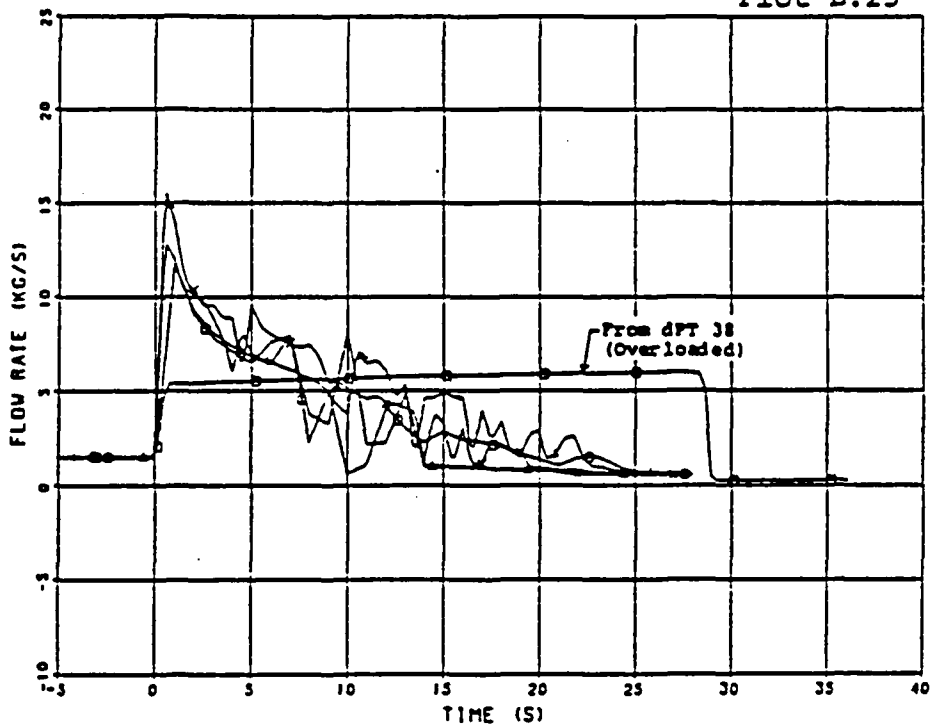
X 000 MASS FLOW RATE. I.L. PUMP - EXPERIMENT
MASS FLOW RATE. I.L. PUMP (FLOWJ 20102) CASE A
MASS FLOW RATE. I.L. PUMP (FLOWJ 20102) CASE B
MASS FLOW RATE. I.L. PUMP (FLOWJ 20102) CASE C
MASS FLOW RATE. I.L. PUMP (FLOWJ 20102) CASE D

Plot B.24



X*P*O D MASS FLOW RATE. S.L. PUMP - EXPERIMENT CASE A
 MASS FLOW RATE. S.L. PUMP (PWLQJ 20202) CASE B
 MASS FLOW RATE. S.L. PUMP (PWLQJ 20202) CASE C
 MASS FLOW RATE. S.L. PUMP (PWLQJ 20202) CASE D

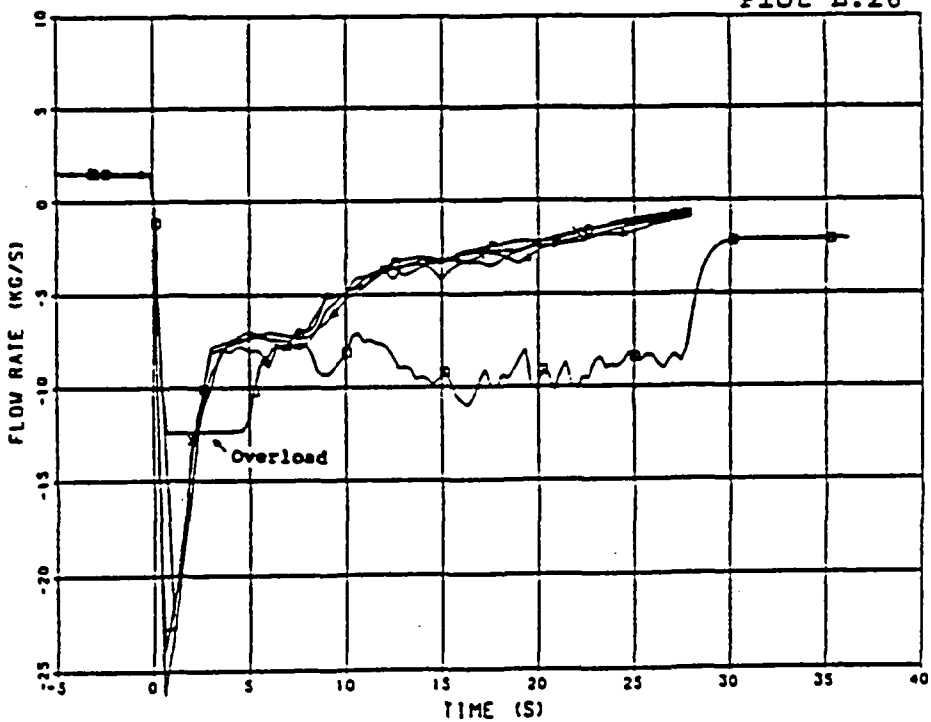
Plot B.25



RELAP5/MOD2 CALCULATION FOR FIX-11. EXP 5061

X*P*O D MASS FLOW RATE. S.L. VESSEL INLET (SPOOL PIECE K10) - EXPER CASE A
 MASS FLOW RATE. S.L. VESSEL INLET (PWLQJ 99011) CASE B
 MASS FLOW RATE. S.L. VESSEL INLET (PWLQJ 99011) CASE C
 MASS FLOW RATE. S.L. VESSEL INLET (PWLQJ 99011) CASE D

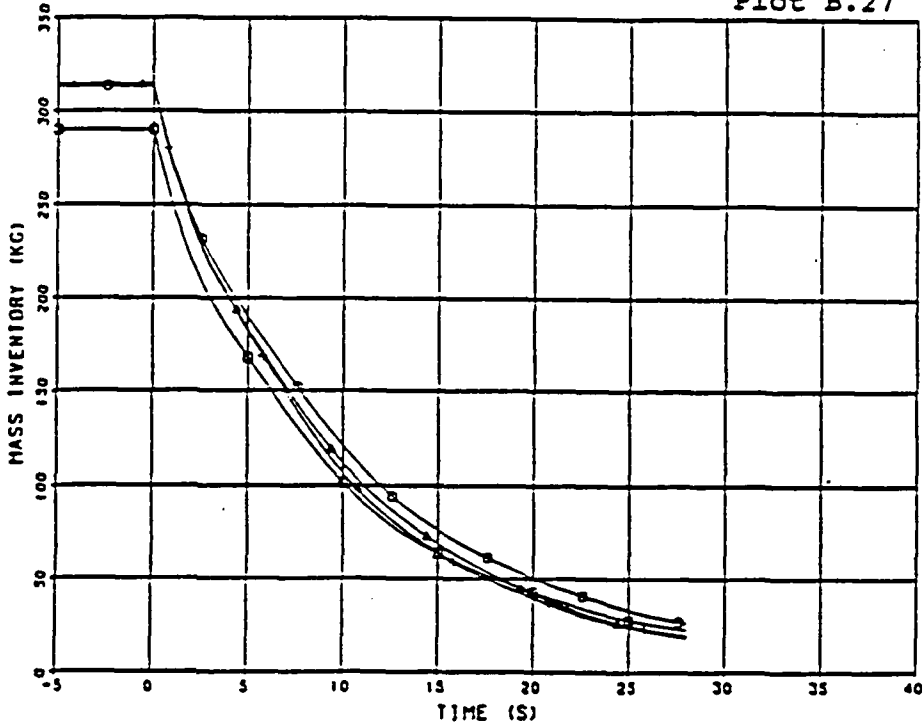
Plot B.26



RELAP5/MOD2 CALCULATION FOR FIX-11. EXP 5061

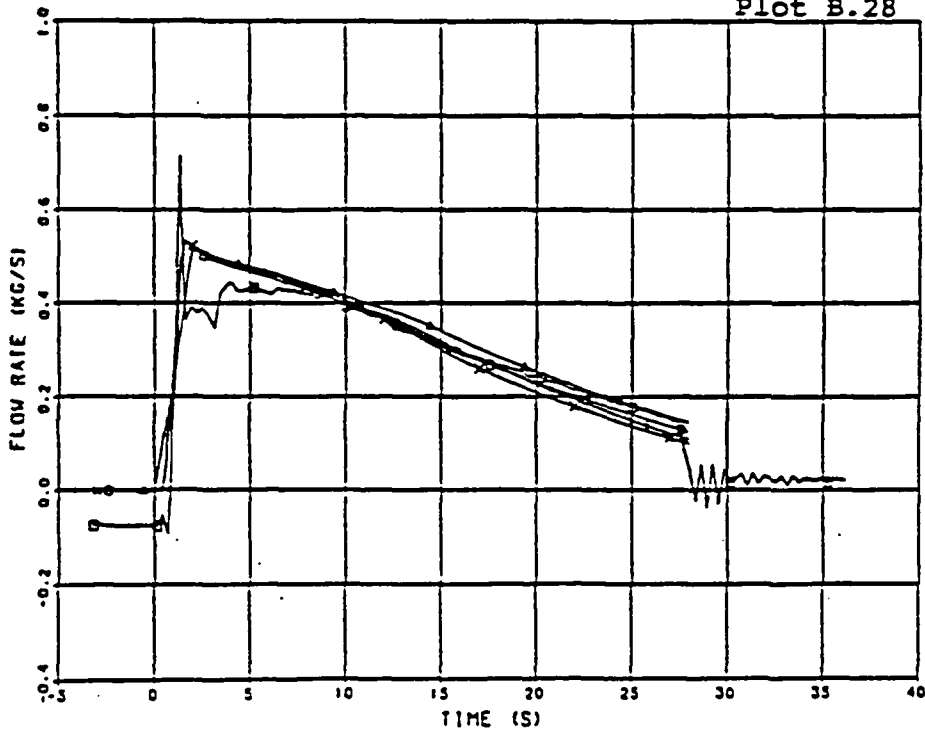
0+00 TOTAL MASS. IN SYSTEM CASE A
0+00 TOTAL MASS. IN SYSTEM CASE B
0+00 TOTAL MASS. IN SYSTEM CASE C
0+00 TOTAL MASS. IN SYSTEM CASE D

Plot B.27



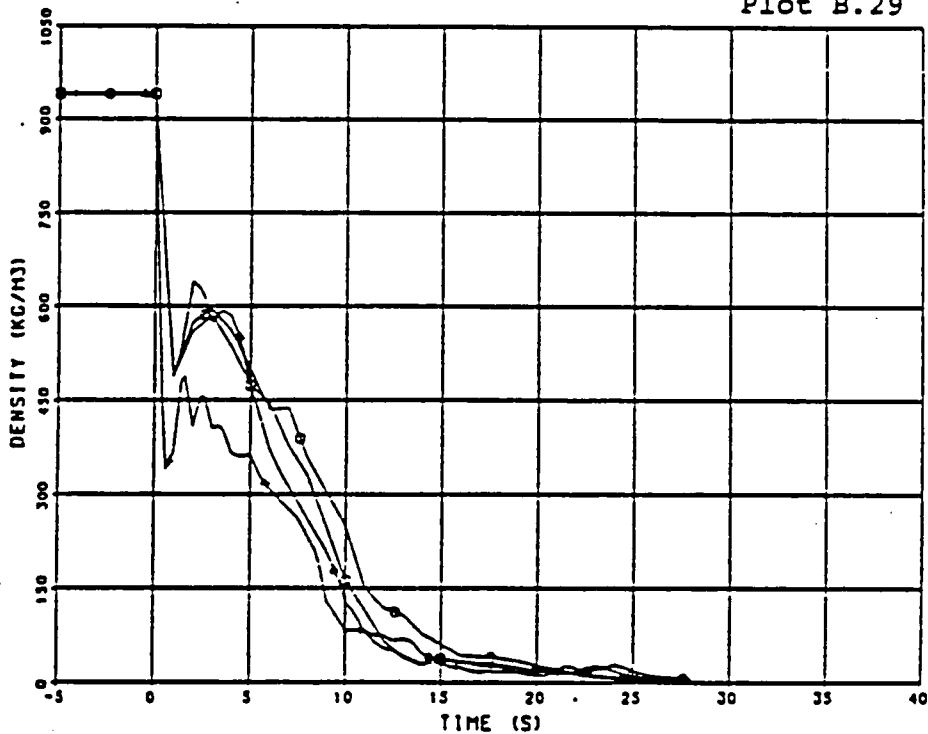
X+00 MASS FLOW RATE. STEAM RELIEF - EXPERIMENT CASE A
X+00 MASS FLOW RATE. STEAM RELIEF (INFLOWJ 404) CASE B
X+00 MASS FLOW RATE. STEAM RELIEF (INFLOWJ 404) CASE C
X+00 MASS FLOW RATE. STEAM RELIEF (INFLOWJ 404) CASE D

Plot B.28



* 000 FLUID DENSITY. BREAK IRMG 96011 CASE A
 * FLUID DENSITY. BREAK IRMG 96011 CASE B
 * FLUID DENSITY. BREAK IRMG 96011 CASE C
 * FLUID DENSITY. BREAK IRMG 96011 CASE D

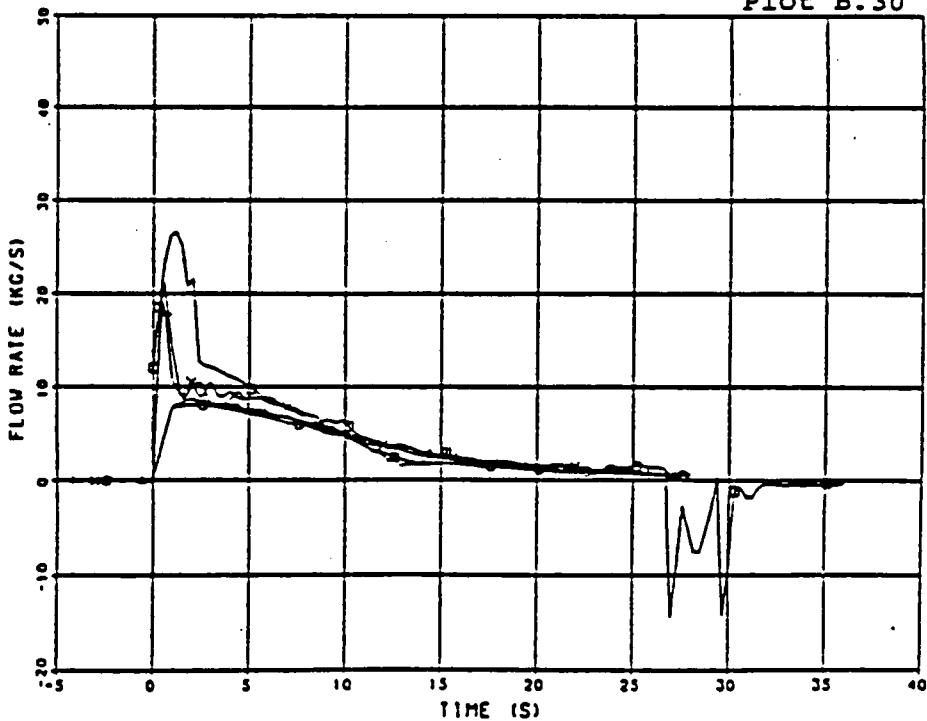
Plot B.29



RELAP5/MOD2 CALCULATION FOR FIX-11. EXP 5061

* 1000 MASS FLOW RATE. BP BREAK FROM T2 INVENTORY - EXPERIMENT
 * MASS FLOW RATE. DC SIDE BREAK (F'FLOWJ 132) CASE A
 * MASS FLOW RATE. DC SIDE BREAK (F'FLOWJ 132) CASE B
 * MASS FLOW RATE. DC SIDE BREAK (F'FLOWJ 132) CASE C
 * MASS FLOW RATE. DC SIDE BREAK (F'FLOWJ 132) CASE D

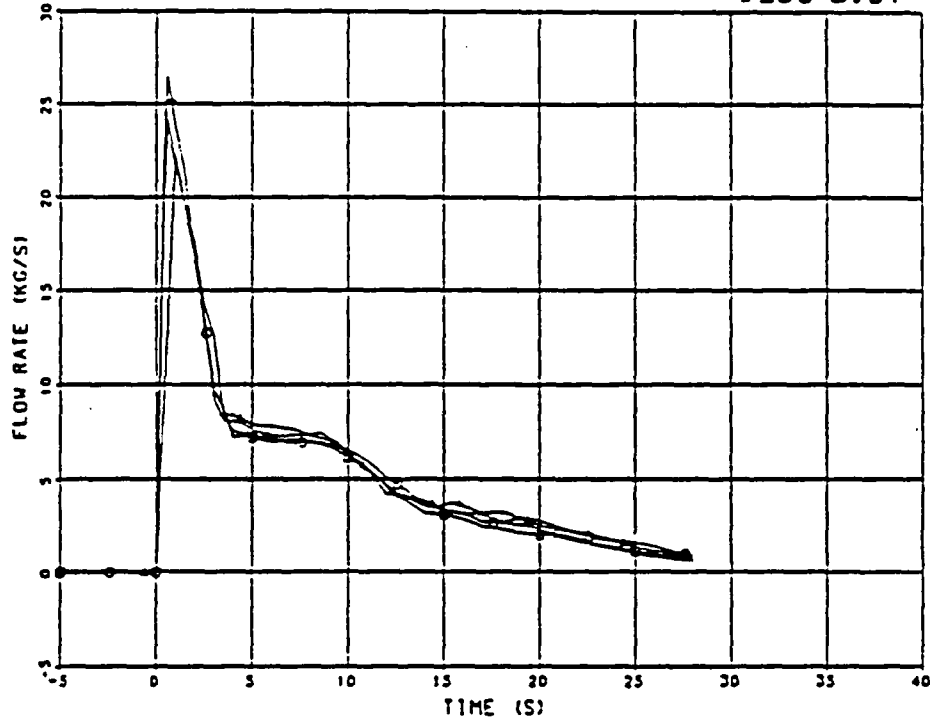
Plot B.30



RELAP5/MD2 CALCULATION FOR FIX-II. EXP 5061

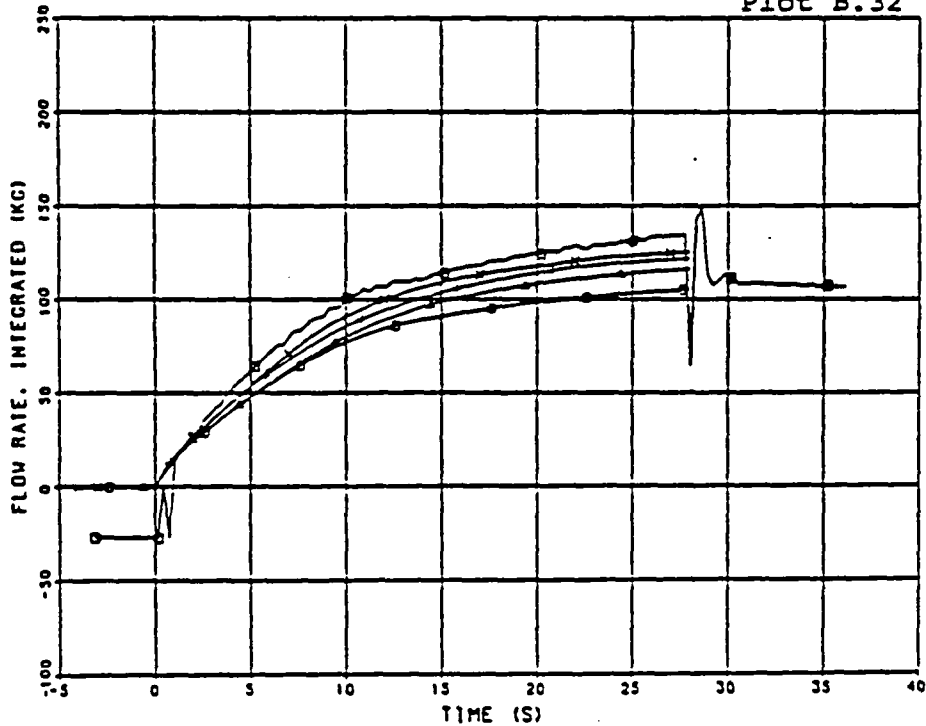
+>00 MASS FLOW RATE. VESSEL SIDE BREAK INFLOWJ 1511 CASE A
MASS FLOW RATE. VESSEL SIDE BREAK INFLOWJ 1511 CASE B
MASS FLOW RATE. VESSEL SIDE BREAK INFLOWJ 1511 CASE C
MASS FLOW RATE. VESSEL SIDE BREAK INFLOWJ 1511 CASE D

Plot B.31



X+>00 MASS LOSS. BREAK FLOW RECEIVER T2 - EXPERIMENT
DC SIDE BREAK TOTAL MASS LOSS (CNTRLVAR 55) CASE A
DC SIDE BREAK TOTAL MASS LOSS (CNTRLVAR 55) CASE B
DC SIDE BREAK TOTAL MASS LOSS (CNTRLVAR 55) CASE C
DC SIDE BREAK TOTAL MASS LOSS (CNTRLVAR 55) CASE D

Plot B.32



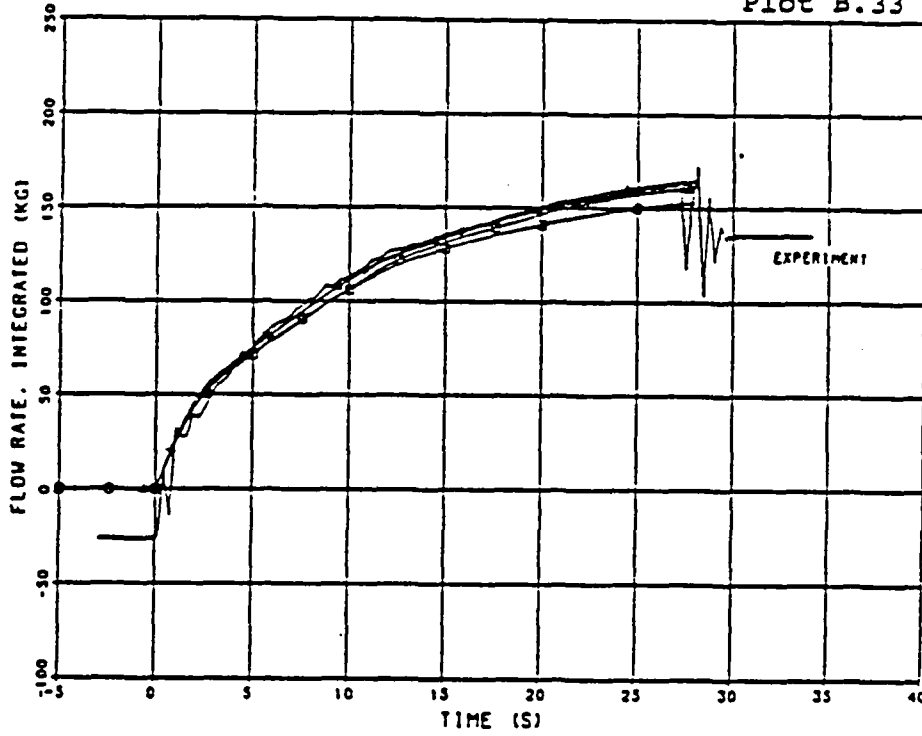

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O O VESSEL SIDE BREAK TOTAL MASS LOSS (CTRLVAR 60) CASE A
O O VESSEL SIDE BREAK TOTAL MASS LOSS (CTRLVAR 60) CASE B
+ O VESSEL SIDE BREAK TOTAL MASS LOSS (CTRLVAR 60) CASE C
+ O VESSEL SIDE BREAK TOTAL MASS LOSS (CTRLVAR 60) CASE D

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RELAPS/MOD2 CALCULATION FOR FIX-II. EXP 5061

Plot B.33

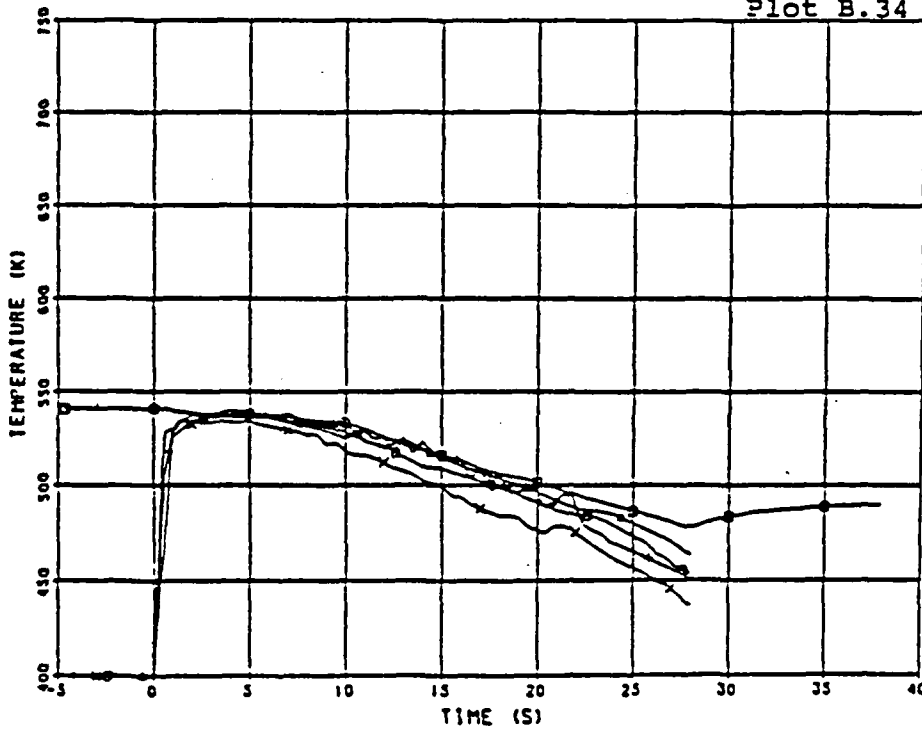


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O O FLUID TEMPERATURE, DC BREAK INLET (TE 34) - EXPERIMENT
O O FLUID TEMPERATURE, BREAK INLET (TEMP 0601) CASE A
O O FLUID TEMPERATURE, BREAK INLET (TEMP 0601) CASE B
+ O FLUID TEMPERATURE, BREAK INLET (TEMP 0601) CASE C
+ O FLUID TEMPERATURE, BREAK INLET (TEMP 0601) CASE D

```

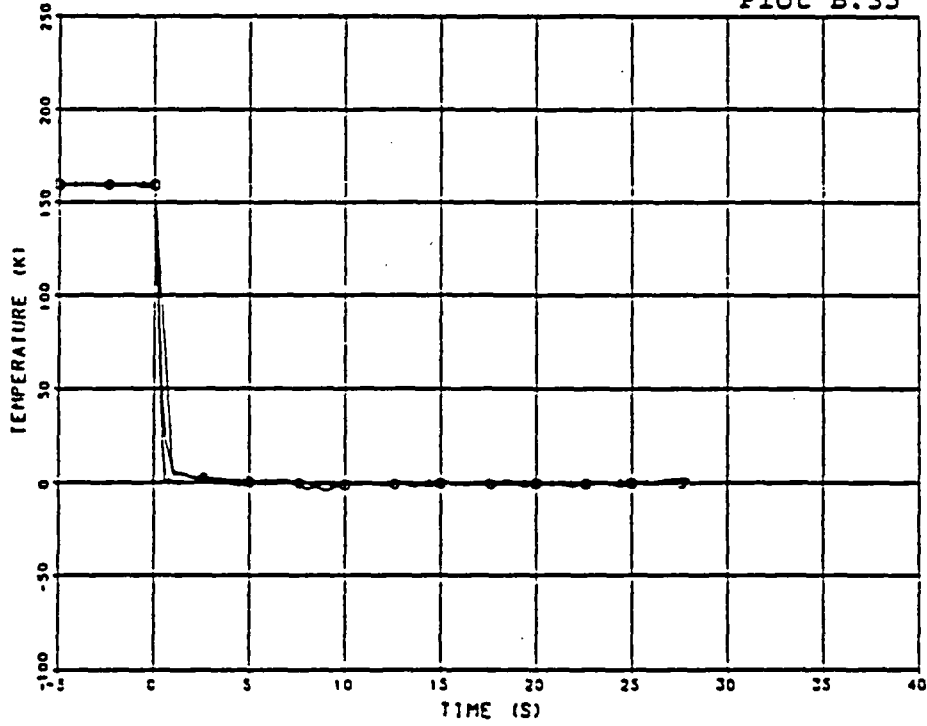
Plot B.34



1986-10-28

* ADD SUBCOOLING. BREAK INLET (TEMP 9101 - TEMP 9101) CASE A
SUBCOOLING. BREAK INLET (TEMP 9101 - TEMP 9101) CASE B
SUBCOOLING. BREAK INLET (TEMP 9101 - TEMP 9101) CASE C
SUBCOOLING. BREAK INLET (TEMP 9101 - TEMP 9101) CASE D

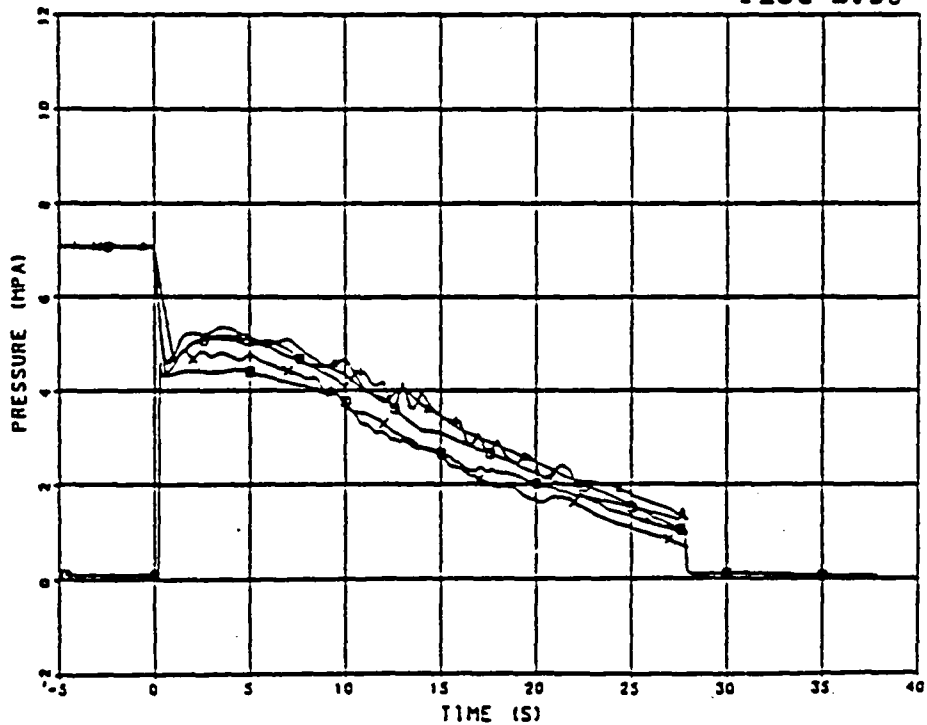
Plot B.35



RELAP5/MOD2 CALCULATION FOR FIX-11. EXP 5061

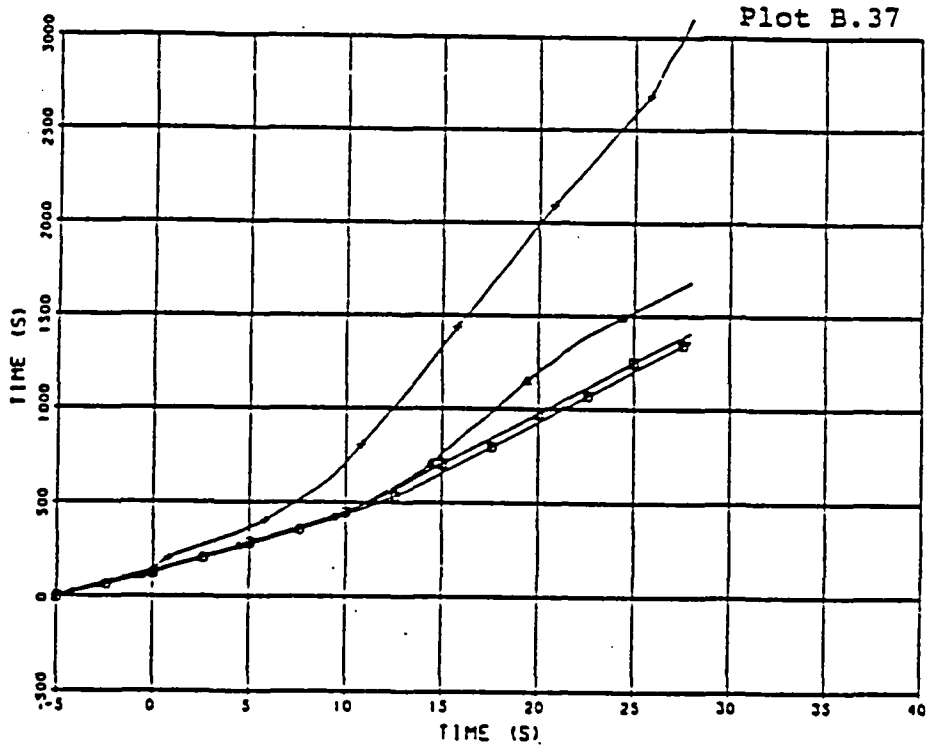
* ADD ..
PRESSURE. DC BREAK INLET (PT 6) - EXPERIMENT
PRESSURE. BREAK INLET (P 9601) CASE A
PRESSURE. BREAK INLET (P 9601) CASE B
PRESSURE. BREAK INLET (P 9601) CASE C
PRESSURE. BREAK INLET (P 9601) CASE D

Plot B.36

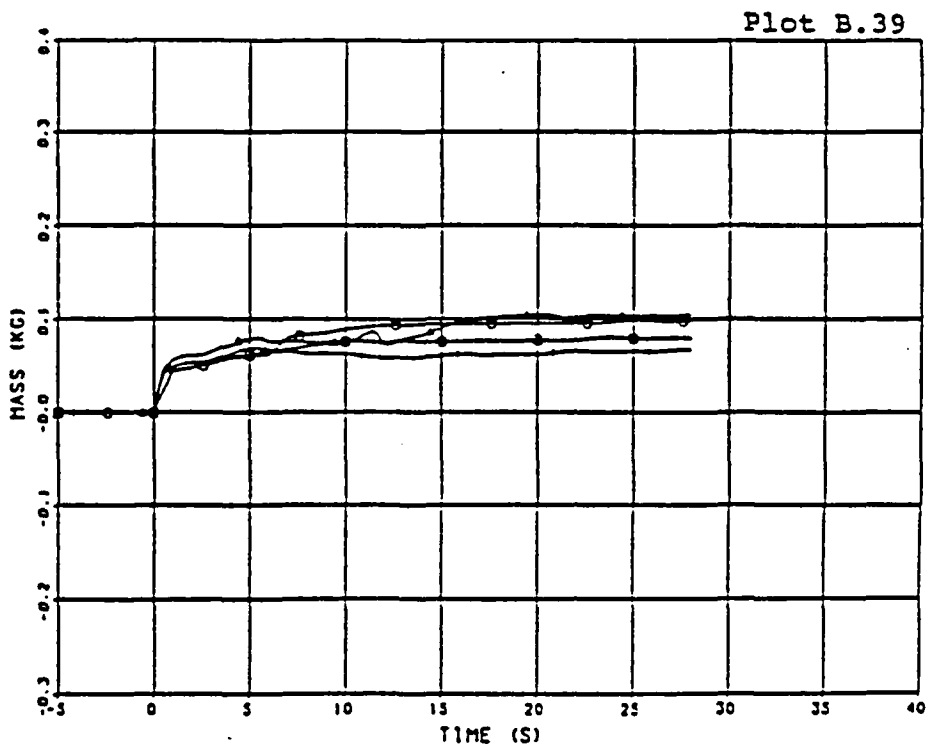


RELAP5/MOD2 CALCULATION FOR FIX-II. EXP 5061

+>00 CPU TIME CASE A
CPU TIME CASE B
CPU TIME CASE C
CPU TIME CASE D



+>00 MASS ERROR CASE A
MASS ERROR CASE B
MASS ERROR CASE C
MASS ERROR CASE D





1986-10-28

APPENDIX C

Calculations to experiment data uncertainties

Case A

 CALCULATION-TO-EXPERIMENT DATA UNCERTAINTY ANALYSIS FOR NRC/ICAP.

FIRST LINE : DIFFERENCE BETWEEN CALCULATED AND (AVERAGED) EXPERIMENTAL DATA AT END OF THE INTERVAL
 SECOND LINE : MEAN DIFFERENCE OVER THE INTERVAL
 THIRD LINE : MEAN SIGMA OVER THE INTERVAL (ROOT MEAN SQUARE OF THE DIFFERENCE)

- CODES -		- - - - TIME INTERVAL - - - -						
CALC.	EXP	0.0 - 2.00	4.000	7.000	10.00	15.00	20.00	27.00
P 1A - P 3		-1.05 -2.05E-01 .694E-01	-1.127 -1.115 .116	-1.170 -1.158 .158	-1.264 -1.224 .227	-1.277 -1.243 .243	-1.383 -1.297 .299	-1.394 -1.381 .381
P 2A - P 4		-1.609E-01 -1.277E-01 -1.363E-01	-1.105 -1.754E-01 -1.784E-01	-1.143 -1.121 .121	-1.238 -1.196 .199	-1.258 -1.217 .210	-1.338 -1.281 .285	-1.356 -1.354 .354
P 3A - P 8		.824 1.81 2.78	.677 .676 .676	.749 .893 .899	.594 .359 .565	.436 .633 .631	.231 .383 .406	-1.110 -1.132 -1.170
PO4A - O 4		-1.727 39.9 54.8	-1.783 -1.29 1.10	2.49 .482 1.01	1.75 3.08 3.10	6.94 4.37 8.50	1.37 8.55 7.47	7.43 8.48 8.37
POLA - O LP		-1.68 -1.17 1.35	-1.978 -1.79 1.81	.203 -1.150 .323	.166 .227 .229	.481E-01 .243E-02 .631E-01	.184 .126 .148	.447 .270 .287
POCA - O CO		-3.41 8.54 11.1	.685 .683 3.70	1.73 -1.83E-01 1.17	.829 1.17 1.40	-1.826 -1.103 3.25	-2.21 -1.48 3.01	.979 -1.324E-01 .617
POLA - O LP		-1.959 -1.152 .636	.200E-02 .610 .897	-1.393 -1.432 .661	-1.181 -1.340 .344	-1.287 -1.488 .638	-1.103 -1.875E-01 .378	-1.922E-01 -1.103 .106
POCA - O CO		1.13 -1.02 4.08	2.27 3.34 4.08	2.78 1.40 1.68	-2.45 -2.08 3.34	.282E-01 .487E-01 1.17	.382 .200 .247	.259 .225 .244
POSA - O SA		-1.83 1.12 4.67	-1.84 -1.295 .796	-1.730 -1.789 .825	-1.639 -1.781 .838	1.24 .985E-01 1.41	-1.400 .813 1.32	-1.807E-02 -1.202 .234
MP1A - X602		.588E-01 .332 .448	.496E-01 .845E-01 .898E-01	.154 1.06 .113	.189 .187 .187	.344 .332 .373	.151 .275 .284	.220 .247 .248
MP2A - X603		-1.122 -1.11 1.40	-1.858 -1.473 .697	-1.823 -1.846 .878	-1.371E-01 -1.874E-01 .248	-1.81 -1.481 .781	-1.31 -1.33 1.41	-1.43 -1.37 1.41
MP3A - X604		4.18 3.24 3.92	1.75 2.71 2.78	2.31 1.62 1.87	-4.14 -1.30 2.14	-3.06 -3.35 3.48	-4.45 -3.87 3.69	-6.35 -4.84 4.86
MP5A - X607		.655E-01 .186E-01 .197	.488E-01 .107 .112	.198E-01 .247E-01 .367E-01	-1.100E-02 .700E-02 .848E-02	.548E-02 .603E-02 .688E-02	-1.121E-01 -1.270E-02 .893E-02	-1.187E-01 -1.148E-01 .148E-01
MP4A - X610		-2.79 -3.18 4.78	4.87 2.32 3.43	4.70 2.80 3.42	3.61 2.17 2.63	6.35 4.76 4.88	7.98 7.11 7.14	7.66 7.51 7.52
MP6A - X636		-12.8 -16.8 17.0	-3.48 -8.30 8.28	-1.82 -2.56 2.84	-1.85 -1.17 1.20	-1.782 -1.144 .838	-1.482 -1.823 .837	18.1 -1.28 1.38
TP1A - T 3		1.25 8.47 8.84	1.82 1.38 1.60	1.14 1.28 1.28	-1.480 .317 .717	-2.04 -1.682 .871	-4.18 -2.89 2.72	-8.88 -8.24 8.37
TP2A - T 14		-2.04 -2.01 3.01	-2.74 -2.82 2.88	-2.77 -2.88 2.88	-2.82 -3.34 3.36	-3.34 -3.27 3.28	-6.94 -4.66 4.74	-10.6 -7.85 7.94
TP4A - T 18		.120 1.20 1.38	-1.200E-01 .301 .381	-1.600 -1.382 .428	-1.48 -1.11 1.20	-2.78 -1.71 1.77	-4.81 -3.51 3.61	-8.11 -6.99 7.08
TP3A - T 31		2.87 1.88 1.72	2.00 3.68 3.78	-1.960 -1.816 1.30	-6.41 -8.88 4.08	-9.60 -7.28 7.38	-13.2 -11.1 11.2	-18.8 -18.7 18.8
TP5A - T 34		-6.51 -68.9 78.8	-1.58 -2.82 3.12	-1.48 -1.21 1.27	-3.41 -2.74 2.83	-6.98 -8.01 6.18	-6.40 -7.31 7.37	-18.9 -11.8 12.2
MT1A - TC 1		7.07 -7.12 3.42	-39.3 -10.3 16.2	-78.9 -65.0 68.8	-88.9 -88.8 80.1	-80.1 108. 83.5	-18.3 -88.8 83.5	-22.5 -14.9 15.3
MT2A - TC 3		-1.38 -7.22 2.18	-18.4 -13.6 14.7	-74.4 -48.2 81.8	-44.2 -60.7 61.4	-104. -93.8 99.2	-68.2 -71.0 73.1	-62.2 -59.3 59.3
MT3A - TC 5		14.4 3.50 6.73	-8.31 1.73 7.89	-6.83 -16.5 16.2	78.7 29.1 38.0	30.0 65.5 89.2	-6.18 19.3 27.4	3.03 -5.04 6.48
MT4A - TC 7		48.8 20.7 26.2	16.7 29.8 31.0	.800 3.31 6.48	36.8 14.9 17.3	42.0 82.9 83.7	-28.2 2.04 31.0	-11.4 -21.7 22.1
MT5A - TC 9		48.3 25.0 29.7	12.4 27.8 28.5	14.3 6.70 7.23	84.2 37.8 41.7	3.13 80.4 83.2	-60.8 -47.1 62.0	-23.9 -26.4 28.1
MT6A - TC12		29.2 21.3 23.8	46.4 44.7 46.3	82.0 43.0 43.6	112. 92.8 83.9	3.01 43.3 88.1	-3.83 -1.09 2.08	-6.72 -6.61 6.73
MT7A - TC18		-1.400E-01 1.35 2.00	-8.31 -2.82 4.82	-8.870 -3.52 4.25	3.23 2.18 3.65	-2.61 -1.80 1.58	-4.73 -3.43 3.53	-13.1 -7.92 8.18
ML1A - X871		-4.98 14.2 20.0	-10.8 -7.80 7.98	-18.1 -18.8 18.8	-20.4 -20.2 20.2	-23.3 -22.8 22.9	-26.0 -24.8 24.8	-29.4 -27.3 27.3
MP1A - X801		.622E-01 -1.41E-02 -1.373E-01	-1.281E-01 .350E-02 .138E-01	-1.713E-02 -1.335E-02 -1.138E-01	-1.768E-02 .379E-02 .783E-02	-1.807E-02 -1.366E-02 .738E-02	-1.237E-02 .287E-02 .581E-02	-1.153E-02 -1.166E-02 .248E-02

1986-10-28

Case B

 CALCULATION-TO-EXPERIMENT DATA UNCERTAINTY ANALYSIS FOR NRC/ICAP.

FIRST LINE : DIFFERENCE BETWEEN CALCULATED AND (AVERAGED) EXPERIMENTAL DATA AT END OF THE INTERVAL
 SECCND LINE : MEAN DIFFERENCE OVER THE INTERVAL
 THIRDO LINE : MEAN SIGMA OVER THE INTERVAL (ROOT MEAN SQUARE OF THE DIFFERENCE)

- CODES -		- - - - TIME INTERVAL - - - -						
CALC.	EXP.	0.0 - 2.00	4.00	7.00	10.00	15.00	20.00	27.00
P 18 - P 3		-.232E-01 .196E-01 .498E-01	-.183E-01 -.101E-01 .184E-01	-.870E-02 -.178E-01 .184E-01	-.687E-01 -.485E-01 .844E-01	.627E-01 .178E-01 .883E-01	-.692E-01 .874E-02 .881E-01	-.148 -.123 .127
P 28 - P 4		.188E-01 .122E-01 .134E-01	-.123E-01 .279E-01 .288E-01	.186E-01 .201E-01 .218E-01	-.408E-01 -.195E-01 .310E-01	-.895E-01 .439E-01 .683E-01	-.471E-01 .228E-01 .874E-01	-.117 -.105 .110
P 38 - P 6		.851 1.83 2.78	.740 .719 .722	.914 .737 .738	.885 .723 .737	.825 .820 .929	.493 .615 .668	.200 .341 .349
PO48 - O 4		-1.40 39.5 84.6	-1.33 -1.74 1.75	-1.70 -1.78 .887	1.79 2.82 2.84	4.62 4.30 8.10	2.40 6.15 8.93	7.27 8.29 8.04
PO58 - O LP		-1.71 -1.18 1.36	-1.00 -1.81 1.84	.172 -.238 .349	.217 .211 .211	.880E-01 .233E-01 .888E-01	.228 .154 .175	.486 .285 .389
PO68 - O CO		-1.21 8.96 11.0	1.48 2.80 3.69	.984 .873 .776	.237 .414 .866	-.842 .974E-01 3.97	-.243 -1.80 2.80	1.17 .409 .873
PO8 - O UP		.106 .874E-01 .801	-.243 1.18 1.32	-.446 -.358 .381	-.250 -.367 .388	-.785 -1.27 1.83	.180 .395 .880	-.958E-01 -.386E-01 .104
PO8 - O DC		.880 -1.17 4.03	1.20 2.84 3.39	-8.01 -1.78 2.89	-.247 -8.30 8.58	-1.17 -2.78 3.33	-1.06 -0.37 1.38	-.236 -.583 8.446
PO38 - O 56		-.402 1.34 4.57	-.611 .328 .884	-.850 -1.68 .891	-1.14 -.952 .894	1.58 -1.49 2.32	-.187 -.386 1.03	-.111 -.133 .328
MP18 - X602		.822E-01 .232 .480	.872E-01 .142 .148	.124 .964E-01 .875E-01	.187 .181 .181	.278 .315 .342	.181 .242 .251	.206 .231 .237
MP28 - X603		-.193 -1.11 1.38	-.831 -.813 .828	-.480E-01 -.303 .339	-.417E-01 .784 .847	-1.54 -1.27E-01 .781	-1.31 -1.14 1.20	-1.34 -1.24 1.29
MP38 - X604		4.26 3.31 4.00	3.01 2.96 3.03	2.12 1.42 1.46	1.58 -3.70 1.66	-4.79 -2.48 3.13	-8.41 -4.93 4.93	-8.41 -6.26 3.26
MP58 - X607		.704E-01 .202E-01 .196	.848E-01 .118 .118	.388E-01 .460E-01 .687E-01	.158E-01 .218E-01 .233E-01	.338E-01 .278E-01 .284E-01	.118E-01 .232E-01 .336E-01	.332E-02 .819E-02 .880E-02
MP48 - X610		-2.88 -3.27 4.89	4.33 1.82 2.74	.788 2.78 3.28	2.89 1.84 1.88	8.22 4.46 4.72	7.37 6.65 8.71	7.37 7.13 7.14
MP68 - X636		-12.3 -18.7 18.9	-3.09 -8.19 8.92	-.886 -2.24 2.32	-1.33 -.808 .827	.808E-01 .820 1.20	-.147 -.221 1.30	15.1 -126 1.30
TF18 - T 3		2.07 8.77 6.18	3.13 2.72 2.74	3.01 2.87 2.88	1.96 2.44 2.48	3.00 2.89 2.96	1.25 2.43 2.56	-1.88 -4.67 1.08
TF28 - T 14		-2.27 -2.80 2.82	-1.48 -1.85 1.81	-.900 -.482 1.31	-.420 -.284 1.25	1.53 .288 .878	-.530 -.210 .889	-2.30 -2.10 2.59
TF48 - T 16		.880 1.61 1.89	1.28 1.37 1.37	1.30 1.22 1.23	.880 1.04 1.08	2.34 1.82 1.88	.880 1.58 1.80	-2.32 -1.24 1.51
TF38 - T 31		2.98 1.71 1.78	2.86 4.09 4.13	1.03 .885 1.29	-2.96 -1.74 1.82	-4.83 -3.61 3.83	-7.78 -6.06 6.18	-11.8 -8.95 10.0
TF58 - T 34		-8.14 -88.8 78.8	-.740 -2.34 2.73	-.280 -.301 .702	-.280 -.387 1.18	-.420 -1.48 3.17	-4.06 -2.28 2.44	-8.28 -6.09 6.24
MT18 - TC 1		4.10 -11.88 3.88	-38.9 -3.88 13.0	-78.5 -43.2 84.0	-86.5 -87.4 87.8	-88.7 -101. 102.	-13.6 -84.1 89.3	-18.2 -8.84 10.1
MT28 - TC 3		18.4 2.84 7.14	10.8 18.8 15.8	-68.0 -18.0 28.0	-22.7 -41.5 43.0	-88.8 -37.8 46.0	-81.8 -83.8 84.8	-60.2 -83.4 93.5
MT38 - TC 5		14.0 3.64 6.88	-11.5 1.85 7.81	-34.5 -28.9 31.0	84.6 3.08 27.1	15.3 88.0 88.7	-2.17 3.87 7.61	-16.7 -6.75 8.33
MT48 - TC 7		40.6 18.5 23.3	2.86 18.8 22.1	-38.4 -25.4 28.8	5.01 -21.0 24.1	12.9 28.3 30.8	-24.3 -24.8 30.4	-30.2 -23.3 23.8
MT58 - TC 9		46.1 25.8 30.7	3.47 22.8 28.2	-15.8 -18.2 17.7	40.8 11.2 22.8	-8.08 34.7 38.0	-47.1 -50.5 83.0	-34.7 -25.7 27.8
MT68 - TC12		17.8 17.4 18.2	-3.41 12.0 14.0	-1.42 -8.34 10.5	58.8 30.8 38.7	4.88 26.7 37.2	.170 2.19 2.86	-6.18 -7.98 3.71
MT78 - TC15		.340 2.20 2.22	-7.25 -3.21 4.11	1.04 -2.06 3.44	22.8 10.2 12.3	2.19 7.83 10.3	.440 1.42 1.63	-6.91 -2.50 3.11
ML18 - X671		-4.83 14.2 20.0	-10.4 -7.36 7.69	-14.8 -14.8 14.8	-17.7 -18.3 18.3	-18.5 -17.8 18.0	-18.2 -15.7 18.7	-18.7 -17.0 17.0
MP18 - X801		.822E-01 -1.141E-02 .373E-01	-.251E-01 -.350E-02 .138E-01	-.712E-02 -.335E-02 -.135E-01	-.786E-02 -.378E-02 .783E-02	-.807E-02 -.386E-02 .738E-02	-.237E-02 -.187E-02 .881E-02	-.193E-02 -.180E-02 .258E-02

1986-10-28

Case C

 CALCULATION-TO-EXPERIMENT DATA UNCERTAINTY ANALYSIS FOR HRC/ICAP

FIRST LINE : DIFFERENCE BETWEEN CALCULATED AND (AVERAGED) EXPERIMENTAL DATA AT END OF THE INTERVAL
 SECOND LINE : MEAN DIFFERENCE OVER THE INTERVAL
 THIRD LINE : MEAN SIGMA OVER THE INTERVAL (ROOT MEAN SQUARE OF THE DIFFERENCE)

- CODES -		- - - - TIME INTERVAL - - - -						
CALC.	EXP.	0.0 - 3.000	4.000	7.000	10.00	15.00	20.00	27.00
P 1C - P 3		-.483E-01 -.472E-02 .644E-01	-.881E-01 -.487E-01 .309E-01	-.817E-01 -.888E-01 .686E-01	-.188 -.103 .110	-.198 -.164 .164	-.408 -.284 .284	-.379 -.493 .499
P 2C - P 4		-.890E-02 .337E-02 .183E-01	-.271E-01 -.891E-02 .128E-01	-.234E-01 -.284E-01 .286E-01	-.128 -.748E-01 .816E-01	-.170 -.134 .134	-.383 -.288 .288	-.350 -.477 .480
P 3C - P 6		.814 1.81 2.84	.927 .867 .868	.888 .745 .750	.330 .484 .446	.850 .837 .957	.823 .804 .836	-.214 -.429E-01 .273
PO4C - O 4		-.334 28.4 38.7	-1.22 -1.84 1.01	1.81 -1.18 1.01	.640 2.18 2.18	3.40 1.54 3.87	1.31 8.27 8.48	6.37 4.35 6.82
POLC - O LP		-1.84 -1.03 1.24	-.897 -1.77 1.80	.182 -.193 .337	-.112E-01 .831E-01 .800E-01	.377E-01 -.412E-01 .828E-01	.201 .142 .168	.406 .281 .278
POCC - O CO		-1.88 2.24 6.78	1.88 1.40 2.36	1.07 .810 1.13	-.787 -.131 1.08	-1.98 -1.31 2.48	-1.77 -2.31 2.88	.886 -.378E-01 .878
POLC - O LP		-.884 -.110 .882	.103 .440 .763	-.418 -.337 .348	-.272 -.373 .374	-.882E-01 -.388 .820	.447E-01 .882E-01 .827E-01	-.106 -.778E-01 -.827E-01
PODC - O DC		.802 2.18 8.63	-1.28 -1.14 4.65	-.882 -1.87 3.95	-4.23 -4.40 4.64	12.0 8.34 11.3	13.4 7.30 8.87	.333 2.78 4.80
PODC - O DC		-.188 -1.23 3.81	-.441 -.288 .718	-.810 -.883 .857	-1.71 -.878 1.02	.148 -.377 1.80	-.838E-01 -.182 .380	.184E-01 -.823E-01 .392
MP1C - M603		.206E-01 .180 .211	.112 .106 .114	.123 .831E-01 .884E-01	.183 .184 .188	.300 .288 .280	.187 .283 .280	.248 .287 .283
MP7C - M603		-.383 -.284 .810	.881E-01 .841E-01 .188	-1.37 -.271 .888	-.837E-01 -.402 .808	-1.77 -.377 1.02	-1.78 -1.48 1.48	-1.54 -1.58 1.83
MP3C - M604		8.08 8.28 8.88	1.28 2.36 3.71	.810 1.28 1.38	-1.74 -.282 .742	-.888 -.883 1.48	-2.83 -2.71 2.82	-8.28 -8.68 4.71
MP8C - M607		.134 .278E-01 .148	.814E-01 .115 .118	.243E-01 .418E-01 .426E-01	.827E-02 -.188E-01 .160E-01	.121E-01 -.128E-01 .134E-01	-.182E-01 -.178E-02 .848E-02	-.318E-01 -.241E-01 .348E-01
MP4C - M618		-4.83 -8.84 7.82	4.38 1.28 2.80	.134 -1.88 2.88	3.83 2.13 2.88	8.32 4.44 4.83	7.72 8.38 8.88	7.50 7.22 7.22
MP8C - M636		-11.8 -10.4 11.0	-2.84 -4.37 8.18	-1.02 -1.71 1.78	-1.81 -.730 .773	-.188E-01 .807 1.11	-.148E-01 -.128 .178	18.1 -.888E-01 1.31
TP1C - T 3		2.38 8.18 8.81	2.71 2.34 2.34	2.41 2.32 2.32	.880 1.77 1.66	-.880 .414 .888	-8.08 -2.78 2.78	-14.2 -8.10 8.80
TP2C - T 14		-2.48 -2.82 2.83	-1.88 -2.32 2.27	-1.48 -1.82 1.83	-1.47 -1.88 1.81	-2.24 -2.88 2.11	-6.78 -4.48 4.87	-18.1 -18.7 11.0
TP4C - T 18		.810 1.82 1.88	.820 1.00 1.02	.710 .870 .883	-.110 .380 .888	-1.47 -.881 .848	-8.88 -3.28 3.88	-14.8 -8.83 10.2
TP3C - T 31		3.82 1.74 1.83	2.88 4.78 4.87	.380 .388 1.08	-2.88 -1.48 2.82	-8.47 -4.23 6.34	-14.3 -11.8 11.2	-24.3 -18.8 18.8
TP8C - T 34		-2.88 -8.88 88.7	1.80 -.280 .878	-2.11 .322 1.82	-8.83 -4.41 4.81	0 -.122 3.22	-3.28 -2.87 3.88	-24.8 -14.8 18.8
MT1C - TC 1		-.808 -2.11 2.58	-48.1 -17.4 23.1	-77.8 -88.1 88.8	-88.8 -88.8 88.2	-88.8 -103. 103.	-18.1 -88.8 83.1	-27.0 -17.1 17.8
MT2C - TC 3		-2.22 -2.78 1.78	-48.8 -27.8 31.8	-118. -88.2 81.3	-110. -122. 122.	-108. -118. 118.	-88.8 -72.2 74.2	-71.4 -82.4 83.4
MT3C - TC 8		84.1 11.2 17.8	17.8 27.8 28.0	14.4 8.28 18.1	88.0 44.7 88.1	-2.81 89.1 71.0	-7.88 -8.78 11.2	-18.7 -13.0 13.7
MT4C - TC 7		87.8 22.4 31.3	28.2 43.1 44.4	2.78 11.8 18.8	38.4 18.7 17.8	18.8 38.8 43.8	-88.0 -48.8 43.7	-38.3 -38.8 38.8
MT8C - TC 8		48.2 21.2 28.4	18.8 28.4 31.0	-.820 -2.82 8.88	48.8 22.8 28.8	-88.0 -7.88 43.8	-84.2 -71.8 72.2	-43.8 -34.1 38.7
MT8C - TC12		32.8 18.8 19.2	33.8 33.8 38.8	12.2 14.1 18.8	72.2 44.2 47.7	1.88 22.2 37.8	-8.18 -2.88 2.88	-18.8 -10.7 11.4
MT7C - TC18		.880 2.48 2.83	-7.72 -2.47 4.40	.870 -2.88 2.78	18.1 8.28 8.87	-1.08 4.28 7.83	-4.08 -2.88 3.18	-17.8 -18.1 18.8
ML1C - M871		-2.88 18.1 28.3	-8.82 -4.27 4.84	-8.48 -8.88 8.77	-12.1 -12.8 12.8	-10.7 -12.7 12.8	-18.8 -10.4 10.4	-12.8 -11.8 11.8
MP1C - M801		.822E-01 .180E-01 .380E-01	-.281E-01 -.848E-02 .178E-01	-.712E-02 -.238E-02 .138E-01	-.288E-02 -.282E-02 .781E-02	-.807E-02 -.431E-02 .823E-02	-.237E-02 -.287E-02 .841E-02	-.183E-02 -.188E-02 .248E-02

Case D

CALCULATION-TO-EXPERIMENT DATA UNCERTAINTY ANALYSIS FOR NRC/ICAP.

FIRST LINE : DIFFERENCE BETWEEN CALCULATED AND (AVERAGED) EXPERIMENTAL DATA AT END OF THE INTERVAL
SECOND LINE : MEAN DIFFERENCE OVER THE INTERVAL
THIRD LINE : MEAN SIGMA OVER THE INTERVAL (ROOT MEAN SQUARE OF THE DIFFERENCE)

- CODES -		- - - - TIME INTERVAL - - - -						
CALC.	EXP	0.0 - 2.000	- 4.000	- 7.000	- 10.00	- 15.00	- 20.00	- 27.00
P 10 - P 3		- .710E-02 -.823E-C2 .308E-01	-.627E-01 -.218E-01 .762E-01	-.861E-01 -.592E-01 -.894E-01	-.258 -.156 .160	-.410 -.295 .299	-.610 -.502 .307	-.702 -.666 .667
P 20 - P 4		.319E-01 .181E-01 .173E-01	-.530E-C2 -.275E-01 .742E-01	-.358E-01 -.178E-01 -.190E-01	-.225 -.176 .140	-.383 -.263 .268	-.588 -.486 .484	-.674 -.648 .649
P 30 - P 6		.370 1.42 2.62	.349 .375 .377	.286 .306 .310	-.940E-02 .141 .193	-.132E-01 .142 .181	-.328 -.188 .218	-.434 -.315 .336
PD40 - D 4		-2.86 23.4 37.1	-2.59 -3.23 3.33	.419 -2.42 2.60	.816 2.59 2.35	8.57 6.83 4.34	2.84 7.70 8.63	7.61 5.88 6.39
POLD - D LP		-2.05 -1.41 1.65	-1.13 -1.96 1.89	-.141 -.407 .466	-.228E-02 -.826E-01 .769E-01	.753E-01 -.291E-01 .447E-01	.197 .153 .171	.422 .260 .277
POCD - D CD		3.37 2.78 6.31	-2.82 -.401 2.73	.181 -.912 1.81	-.334 -.184 .635	-1.13 -2.43 2.93	-1.17 -1.00 1.89	.883 -.134 .969
POLD - D LP		.712 .126 .419	-.543 .534E-01 .693	-.467 -.510 .531	-.121 -.362 .386	-.485 -.732 .897	-.115 -.870E-01 .124	-.126 -.174 .126
POOD - D DC		-.427 -1.62 3.99	-.240E-01 2.83 3.06	-1.21 -3.83 4.71	-2.13 -.602 1.18	.262 -.896 1.15	-.324 .468 1.16	.196 -.274 .415
POSD - D S6		1.51 .615 3.17	-1.32 -.483 .911	-.863 -.853 .820	-.498 -.899 .932	-.821 -.647 1.84	-.180 -.305 .377	-.212 -.232 .272
MP10 - X602		.174E-01 .120 .194	.477E-01 .294E-01 .813E-01	.112 .687E-01 .739E-01	.203 .174 .176	.349 .334 .341	.202 .301 .310	.266 .285 .290
MP20 - X603		-.302 -.399 .758	-.238 -.376 .378	-.238 -.229 .271	-.466 .801E-01 .388	1.82 -.127 .891	-1.58 -1.44 1.48	-1.47 -1.44 1.47
MP30 - X604		4.93 4.82 8.42	3.39 4.38 4.11	2.89 2.55 2.65	-.397 1.01 1.35	-2.31 -1.68 1.93	-4.95 -3.95 4.00	-6.43 -5.27 6.27
MP50 - X607		.138 .375E-01 .147	.838E-01 .116 .434E-01	.239E-01 .427E-01 .434E-01	-.810E-03 .123E-01 .149E-01	-.870E-02 .164E-02 .480E-02	-.330E-01 -.200E-01 .216E-01	-.418E-01 -.382E-01 .383E-01
MP40 - X610		-2.12 -7.84 9.08	4.36 2.51 3.28	.159 2.58 3.21	3.42 1.82 2.20	8.51 4.53 4.68	7.83 6.82 6.84	7.80 7.81 7.82
MP60 - X636		-11.0 -11.7 12.2	-1.99 -3.89 4.78	.179 -.896 1.11	-1.44 .875E-02 .819	-.184 .618 1.06	-.384 -.417 .630	15.0 -1.18 1.33
TF10 - T 3		2.86 6.38 8.72	2.88 2.24 3.54	2.36 2.38 3.00	-.380 1.19 1.89	-4.10 -1.44 1.78	-8.12 -4.23 6.46	-18.2 -13.3 13.6
TF20 - T 14		-2.14 -2.32 2.35	-1.82 -1.89 1.94	-1.53 -1.69 1.70	-2.66 -2.48 2.36	-6.55 -3.91 3.98	-10.9 -8.31 8.47	-20.1 -14.9 18.2
TF40 - T 18		.860 1.87 1.78	1.06 1.27 1.28	.680 .795 .810	-1.36 -.244 .816	-4.80 -2.39 2.88	-8.79 -7.17 7.37	-18.7 -14.1 14.3
TF30 - T 31		7.18 3.52 4.07	2.72 4.91 5.17	.700E-01 .308 1.14	-6.32 -3.24 3.46	-11.6 -7.83 8.13	-18.2 -14.8 14.9	-28.3 -22.8 23.0
TF50 - T 34		-4.93 -38.0 62.1	-4.06 -4.30 4.35	-6.53 -4.78 4.89	-12.6 -6.98 8.19	-18.9 -14.3 14.3	-24.3 -20.3 20.4	-33.6 -25.9 26.3
MT10 - TC 1		1.87 -2.80 3.60	-28.2 -4.86 8.63	-26.8 -81.0 62.3	-87.7 -87.9 88.1	-81.7 -105. 105.	-23.0 -42.1 64.3	-30.8 -21.2 21.5
MT20 - TC 3		8.98 1.51 4.34	16.8 11.6 12.0	-.870 12.2 14.4	18.1 7.66 10.3	-89.8 -40.4 84.1	-61.0 -71.0 72.7	-82.1 -61.3 61.4
MT30 - TC 6		-1.73 .858 1.80	-29.5 -27.4 29.5	-26.6 -40.8 63.0	-76.6 -37.2 46.8	-70.8 -27.2 84.4	-14.9 -24.8 29.3	-6.52 -13.4 13.9
MT40 - TC 7		-.360 2.64 3.42	-85.8 -80.8 87.6	-184. -138. 139.	-116. -150. 160.	-85.3 -122. 123.	-39.3 -64.8 66.6	-24.3 -32.5 32.8
MT50 - TC 8		29.0 15.3 20.3	-30.8 .847 17.6	-141. -87.7 86.2	-65.8 -106. 109.	-107. -110. 112.	-61.5 -61.8 62.3	-28.1 -33.8 35.4
MT60 - TC12		6.62 10.5 12.7	-2.99 10.8 12.9	-3.40 -10.3 11.1	42.2 27.6 32.7	-2.80 3.12 10.5	-9.62 -6.50 6.74	6.46 -6.00 8.03
MT70 - TC15		.800 2.32 2.34	-7.46 -3.35 4.29	.320 -2.42 3.60	8.61 7.73 8.47	-3.94 -.485 3.60	-8.07 -8.40 8.62	-1.41 -9.11 9.73
ML10 - X671		-3.77 15.1 20.7	-6.36 -4.75 4.88	-6.51 -8.35 8.48	-6.82 -8.35 8.39	-6.37 -7.16 7.46	-6.92 -5.88 6.92	-8.41 -7.46 7.82
MP10 - X801		.822E-01 1.00E-01 .290E-01	-.251E-01 -.849E-02 .175E-01	-.713E-02 -.328E-02 .138E-01	-.768E-02 -.282E-02 .791E-02	-.807E-02 -.435E-02 .823E-02	-.237E-02 .367E-02 .681E-02	-.153E-02 -.152E-02 .243E-02

1986-10-28

APPENDIX D

Description of the accompanying data package

STUDSVIK

THIS TAPE CONTAINS DATA FROM THE ICAP PREDICTION CALCULATION
WITH THE RELAP5/MOD2/36.04 FOR THE FIX-II EXPERIMENT NO. 5061.

CONTENTS, FILE	1.	THIS DESCRIPTIVE TEXT
	2.	INPUT CASE A, STEADY STATE
	3.	- " - A, TRANSIENT
	4.	- " - B, STEADY STATE
	5.	- " - C, - " -
	6.	- " - D, - " -
	7.	DATA, EXPERIMENT
	8.	- " - , CASE A
	9.	- " - , CASE B
	10.	- " - , CASE C
	11.	- " - , CASE D

I. COMPUTER

NAME	CYBER 170-810
WORD SIZE	60

II. TAPE FORMAT

NUMBER OF TRACKS	9
PACKING DENSITY	1600 BPI
RECORD SIZE	80
BLOCKING FACTOR	64
CODED	EBCDIC
CONTROL WORDS	NO

III. DATA FORMAT, FOR EACH OF THE FILES 5 THROUGH 8

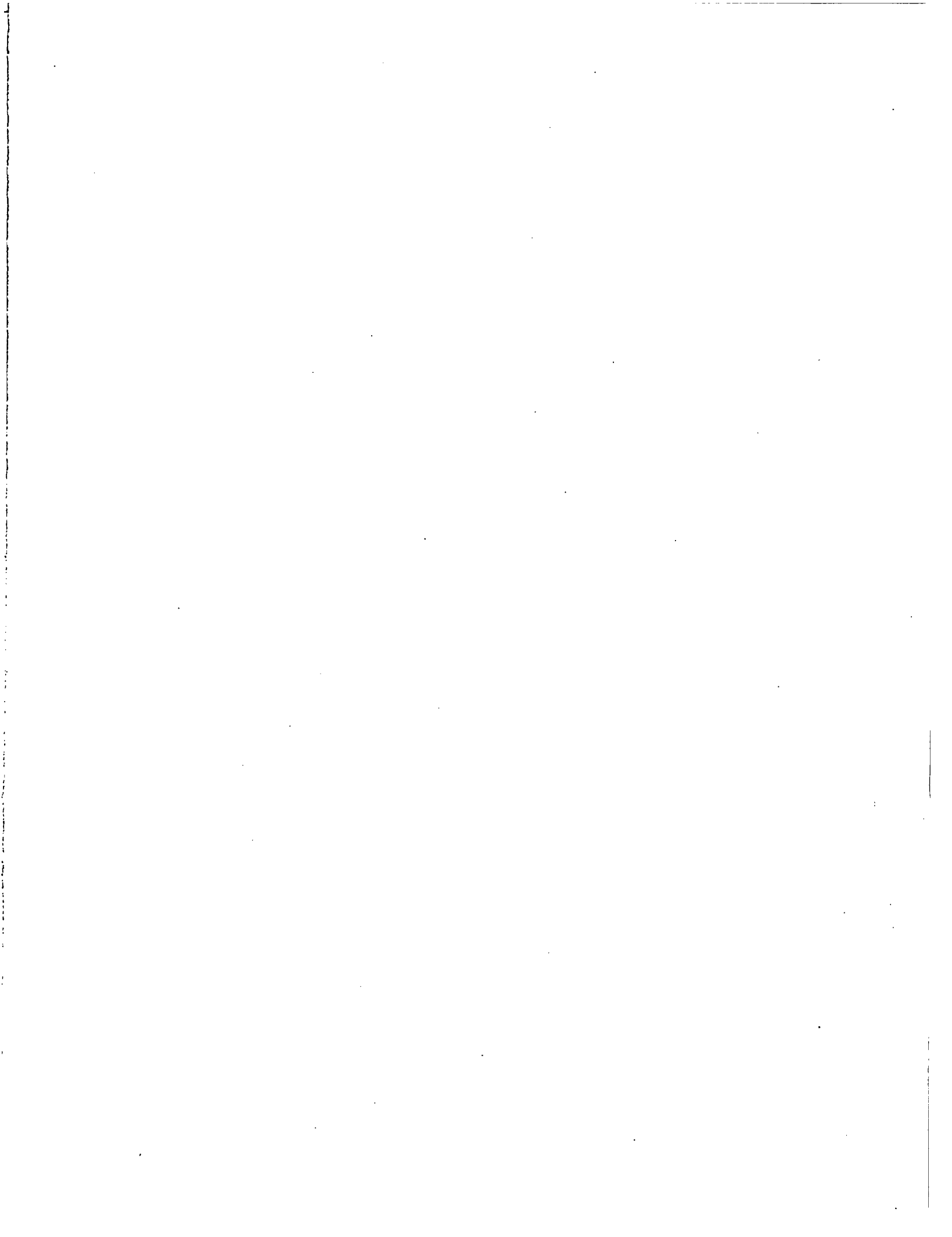
TITLE RECORD(S), (FORMAT I5.A75)
FIELD 1, THE NUMBER OF DATA CHANNELS ON THE FILE
FIELD 2, PROBLEM IDENTIFICATION
UP TO FIVE ADDITIONAL IDENTIFICATION RECORDS
MAY BE ADDED BY 'C' IN COLUMN 1 OF FIELD 1

DATA SET RECORD 1, (FORMAT 2I5.A60)
FIELD 1, NUMBER OF DATA POINTS
FIELD 2, THE ENGINEERING UNIT CODE (EUC) FOR THE
VARIABLE
FIELD 3, IDENTIFYING TEXT OF THE DATA
REMAINING DATA SET RECORDS FORMAT 5(E16.9)

EACH DATA CHANNEL SUBMITTED IS GIVEN THROUGH TWO DATA
SETS, THE FIRST OF WHICH IS THE TIME DATA SET.
THE TWO SETS HAVE THE SAME NUMBER OF DATA POINTS.
THE TIME DATA SET IS IDENTIFIED BY EUC-77 (FIELD 2)
AND THE IDENTIFYING TEXT 'TIME' (FIELD 3).

NRC FORM 338 (2-84) NRCM 1102, 3201, 3202 BIBLIOGRAPHIC DATA SHEET SEE INSTRUCTIONS ON THE REVERSE	U.S. NUCLEAR REGULATORY COMMISSION 1 REPORT NUMBER (Assigned by TIDC and Vol. No., if any) NUREG/IA-0016 STUDSVIK/NP-86/109
2 TITLE AND SUBTITLE Assessment of RELAP5/MOD2, Cycle 36.04 Against FIX-II Guillotine Break Experiment No. 5061	3 LEAVE BLANK 4 DATE REPORT COMPLETED MONTH YEAR
5 AUTHOR(S) John Eriksson	6 DATE REPORT ISSUED MONTH YEAR July 1989
7 PERFORMING ORGANIZATION NAME AND MAILING ADDRESS (Include Zip Code) Swedish Nuclear Power Inspectorate P.O. Box 27106 S-102 52 Stockholm, Sweden	8 PROJECT/TASK/WORK UNIT NUMBER 9 FIN OR GRANT NUMBER
10 SPONSORING ORGANIZATION NAME AND MAILING ADDRESS (Include Zip Code) Office of Nuclear Regulatory Research U.S. Nuclear Regulatory Commission Washington, DC 20555	11a TYPE OF REPORT Technical Report 11b PERIOD COVERED (inclusive dates)
12 SUPPLEMENTARY NOTES	
13 ABSTRACT (200 words or less) <p>The FIX-II guillotine break experiment No. 5061 has been analyzed using the RELAP5/MOD2 code. The code version used, Cycle 36.04, is a frozen version of the code.</p> <p>Four different calculations were carried out to study the sensitivity of initial coolant mass, junction operations and break discharge line nodalization. The differences between the calculations and the experiment have been quantified over intervals in real time for a number of variables available from the measurements during the experiment.</p> <p>The break mass flows were generally underpredicted at the same time as the depressurization rate was overpredicted.</p>	
14 DOCUMENT ANALYSIS • KEYWORDS/DESCRIPTORS RELAP5/MOD2, ICAP Program, FIX-II, Guillotine Break 15 IDENTIFIERS/OPEN ENDED TERMS	15 AVAILABILITY STATEMENT Unlimited 16 SECURITY CLASSIFICATION (This page) Unclassified (This report) Unclassified 17 NUMBER OF PAGES 18 PRICE





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