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ADVISORY COMMITTEE ON REACTOR SAFEGUARDS

April 25, 2006

The contents of this transcript of the proceeding of the United States Nuclear Regulatory Commission Advisory Committee on Reactor Safeguards, taken on April 25, 2006, as reported herein, is a record of the discussions recorded at the meeting held on the above date.

This transcript has not been reviewed, corrected and edited and it may contain inaccuracies.

1 UNITED STATES OF AMERICA
2 NUCLEAR REGULATORY COMMISSION

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4 ADVISORY COMMITTEE ON REACTOR SAFEGUARDS
5 MEETING OF THE SUBCOMMITTEE ON POWER UPRATES

6 + + + + +

7 BEAVER VALLEY POWER STATION EXTENDED POWER UPRATE

8 + + + + +

9 TUESDAY, APRIL 25, 2006

10 + + + + +

11 The subcommittee meeting convened at the
12 Nuclear Regulatory Commission, Two White Flint North,
13 Room T-2B3, 11545 Rockville Pike, at 8:30 a.m.,
14 Richard B. Denning, Chair, presiding,

15
16 SUBCOMMITTEE MEMBERS PRESENT:

17 RICHARD B. DENNING, Chair

18 SANJOY BANERJEE ACRS Consultant

19 THOMAS S. KRESS

20 OTTO L. MAYNARD

21 JOHN D. SIEBER

22 GRAHAM B. WALLIS

23 ACRS STAFF PRESENT:

24 RALPH CARUSO

25

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FIRSTENERGY STAFF PRESENT:

A.R. BURGER	FENOC
MATT CERRONE	Westinghouse
DON DURKOSH	FENOC
KEN FREDERICK	FENOC
DAVID FINK	Westinghouse
CHUN FU	Westinghouse
NORM HANLEY	Stone & Webster
JOSH HARTZ	Westinghouse
GREG KAMMERDINER	FENOC
BRETT KELLERMAN	Westinghouse
JAMES LASH	FENOC
MARK MANOLERAS	FENOC
CHRIS MCHUGH	Westinghouse
BRIAN MURTAGH	FENOC
MAHESH PATEL	FENOC
JACK PENKROT	Westinghouse
PETE SENA	FENOC
GEORGE STORLIS	FENOC
MIKE TESTA	FENOC
DENNIS WEAKLAND	FENOC

NRR STAFF PRESENT:

TIMOTHY COLBURN

RICHARD LOBEL

JIM MEDOF

SAMUEL MIRANDA

JOHN PARILLO

PAT PATNAIK

LYNN WARD

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P-R-O-C-E-E-D-I-N-G-S

8:32 a.m

CHAIRMAN DENNING: The meeting will now come to order. This is a meeting of the Advisory Committee on Reactor Safeguards Subcommittee on Power Uprates. I'm Richard Denning, Chairman of the Subcommittee.

Subcommittee members in attendance are Tom Kress, Otto Maynard, Jack Sieber, Graham Wallis who is virtually at the moment, but will be physically here later and our consultant Sanjoy Banerjee, who also seems to be virtually here.

The purpose of this meeting is to discuss the extended power uprate application for the Beaver Valley Power Station. The Subcommittee will hear presentations by and hold discussions with representatives of the NRC Staff and the Beaver Valley Power Station licensee, FirstEnergy, regarding these matters.

The Subcommittee will gather information, analyze relevant issues and facts and formulate proposed positions and actions as appropriate for deliberation by the full Committee. Ralph Caruso is the designated federal official for this meeting.

The rules for participation in today's

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1 meeting have been announced as part of the notice of
2 this meeting previously published in the *Federal*
3 *Register* on April 12, 2006.

4 A transcript of the meeting is being kept
5 and will be made available as stated in the *Federal*
6 *Register* notice.

7 It is requested that speakers first
8 identify themselves and speak with sufficient clarity
9 and volume so that they can be readily heard.

10 We have received any requests from members
11 of the public to make oral statements or written
12 comments.

13 We think that the agenda that we're going
14 through today and tomorrow is quite well balanced
15 towards addressing the principal interests and
16 interests of the Subcommittee. We know that the power
17 uprates will result in some eating into safety
18 margins. WE need to know where that's occurring and
19 become convinced that the margins are still adequate.

20 This is a very quantitative Committee. The
21 Staff's review of the application must be
22 comprehensive, our view must in many sense be in many
23 aspects be more focused. We'd like you to spend
24 minimal time on the aspects of plant safety that are
25 not effected by the uprate. The nice thing about

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1 having the safety analysis results today is that there
2 is always tomorrow to ask you to come back and give us
3 more detail.

4 You'll notice our room has been modified
5 somewhat over the last couple of weeks. I hope that
6 everything's going to work okay. I know the screen
7 isn't perfect, but we will proceed.

8 Now I would like to turn the meeting over
9 to Mr. Colburn of the NRC Staff to begin.

10 MR. COLBURN: Thank you, Mr. Denning.

11 My name is Tim Colburn. I am a Senior
12 Project Manager in the Division of Operating Reactor
13 Licensing in the Office of Nuclear Reactor Regulation.
14 I'm assigned to the Beaver Valley Power Station, Units
15 1 and 2.

16 During the next two days presentations
17 will be made by the Staff and the licensee concerning
18 background information related to the application,
19 plant changes associated with the application and fuel
20 and core design changes, safety analysis including
21 methodology used for conducting those safety analysis,
22 discussion of non-LOCA events and large break LOCA.

23 The Staff and licensee will conduct
24 discussions of the safety analysis.

25 The safety analysis discussion will also

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1 include discussions by licensee and the Staff on small
2 break LOCA, long term cooling and boron precipitation,
3 containment over pressure credit and dose analyses.

4 The Staff will also provide a discussion
5 of the containment analysis associated with the
6 conversion from sub-atmospheric to atmospheric
7 conditions and its dose analysis and implementation of
8 the alternative source term.

9 CHAIRMAN DENNING: I think you can just
10 arrow down, Tim, if you want to there.

11 MR. COLBURN: The Staff and the licensee
12 will also discuss the materials and reactor vessel
13 integrity issue associated with the safety evaluation
14 for the power uprate.

15 On day two a discussion of the balance of
16 plant issues associated with the power uprate, flow
17 accelerate corrosion, vibration, corrosion erosion and
18 risk evaluation will be conducted by both the Staff
19 and the licensee.

20 Operations and testing associated with the
21 power uprate including human factor issues, power
22 ascension testing and the licensee test plan for
23 basically what amounts to a two phrase implementation
24 of the testing will be discussed. And then conclusions
25 of the licensee and the Staff.

1 The licensee had several license amendment
2 applications that they had submitted prior to the
3 power uprate which were needed to support the power
4 uprate review. These included:

5 Steam generator allowable value setpoint
6 changes, which were to eliminate concerns the Staff
7 had with measurement uncertainty;

8 A containment conversion license amendment
9 application to convert the Beaver Valley Power Station
10 1 and 2 containments from sub-atmospheric to
11 atmospheric conditions;

12 Best estimate LOCA methodology approval
13 for the large break LOCA analyses;

14 Steam generator replacement for Beaver
15 Valley Power Station Unit 1 only. Replace the previous
16 steam generators with the Model 54F steam generators;
17 and

18 Implementation of the relaxed axial offset
19 control methodology for both units.

20 These amendments have all been approved
21 and all have been implemented for Unit 1.
22 Implementation of some of these will be for Unit 2 in
23 the fall of 2006 outage.

24 The licensee's submittal originally was
25 sent in on October 4, 2004. It had numerous

1 supplements. The licensee had submittals on February
2 23rd and June 14 of 2005 which were necessary to
3 consider the application a complete application. The
4 Staff issued its acceptance review of the licensee's
5 application in July of 2005 and indicated that it
6 would be reviewing the application for basically
7 within a one year time frame.

8 The licensee's application requested an
9 increase in reactor power from the current 2689
10 megawatts thermal to 2900 megawatts thermal. This is
11 approximately an 8 percent increase in power and is
12 considered an extended power uprate.

13 The Staff plans to issue its safety
14 evaluation and amendment on or about the end of June
15 2006. The licensee plans to implement the extended
16 power uprate for Unit 1 within 120 days of receipt of
17 the approval. And for Unit 2 in a phased approach
18 concluding with the completion of balance of plant
19 upgrades including a turbine upgrade in the spring of
20 2008.

21 What I'd like to do now is turn the
22 presentation over to the licensee's site Vice
23 President Mr. Jim Lash for his opening remarks.

24 MR. LASH: First off, my name is Jim Lash.

25 CHAIRMAN DENNING: No. Hold on just a

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1 second.

2 MR. LASH: Okay. First off, my name is
3 Jim Lash, site Vice President of Beaver Valley Power
4 Station.

5 Good morning, Mr. Chairman and
6 distinguished members, ACRS consultants. This morning
7 I'd like to provide a brief introduction and some
8 background to the Beaver Valley power uprate. Our
9 decided outcome is to provide you with sufficient
10 information and answer all relevant questions
11 regarding the Beaver Valley power uprate so that you
12 can form appropriate decisions and recommendations to
13 the NRC Commissioners.

14 We've built this presentation to cover a
15 number of areas effected by the uprate in areas that
16 we believe are of interest to the Committee in
17 fulfilling the desired outcome of these proceedings.

18 We have a full agenda of items to cover in
19 the next two days, and that is shown here on this
20 slide.

21 I'd like to introduce the presenters from
22 FENOC. Other than myself will be Pete Sena will
23 provide an overview. He is the Director of Engineering
24 at Beaver Valley.

25 Mark Manoleras on plant changes. He is

1 the Design Engineering Manager at Beaver Valley.

2 A.R. Burger will do reactor fuel and core
3 design. He is a supervisor of core design.

4 Ken Frederick will address safety
5 analysis. He is a nuclear safety analyst.

6 Dennis Weakland materials and reactor
7 vessel integrity. He's a fleet material
8 representative.

9 Mike Testa the mechanical plant VOP. He's
10 the EPU Project Manager.

11 Risk evaluation Colin Keller, who is the
12 supervisor of the PRA group at Beaver Valley.

13 And finally the operations and testing
14 aspects of this project will be Don Durkosh, who is a
15 senior reactor operator.

16 Each presenter will describe their area of
17 expertise and introduce any subject matter experts
18 that they'll use during the course of their
19 presentation and at the time of their presentation.

20 In addition to the presenters we have
21 subject matter experts here from Beaver Valley as well
22 as some contractors, organizations supporting us,
23 Westinghouse and Stone & Webster.

24 The balance of my comments will briefly
25 focus on the history of Beaver Valley, the extended

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1 power uprate time line, the peer units experienced
2 with power uprate and the oversight of our power
3 uprate project.

4 Okay. Beaver Valley units are three loop
5 Westinghouse PWRs that achieved commercial operations
6 in 1976 for 1776 Unit 1 and 1987 for Unit 2. The
7 original core licensed power was 2652 megawatts
8 thermal or 2660 megawatts thermal NSSS power. And
9 both units have currently implemented a 1.4 percent
10 uprate to 2689 megawatt thermal or 2697 megawatt
11 thermal NSSS power. This uprate credited the improved
12 feedwater flow measurements implemented in the fall of
13 2001.

14 CHAIRMAN DENNING: Let me ask you just a
15 couple of questions related to the differences between
16 the two designs. Obviously there's a long distant
17 time differential between when the two were started.
18 But even before we get into the steam generator
19 replacement there are some fairly significant
20 differences. And you have, I gather, separate
21 simulators for the two. Can you give me just a little
22 feeling as to what the principal differences are just
23 at this point prior to?

24 MR. LASH: Well, they're principally the
25 same design, however there is a time difference

1 between the implementations of those units so there is
2 a difference in some aspects of the systems for both
3 units.

4 CHAIRMAN DENNING: Yes.

5 MR. LASH: We do qualify operators
6 independently for those two units, so we have dual
7 simulators to maintain a bank of SROs qualified
8 personnel for each unit. We're not dual licensed on
9 the plant.

10 The specific design aspects I think we'll
11 get into in the safety analysis and how we've treated
12 those differences later on with some of the other
13 presenters.

14 CHAIRMAN DENNING: Yes. But the operators
15 are licensed to operate just one or the other unit?

16 MR. LASH: That is correct?

17 CHAIRMAN DENNING: And do some of them
18 learn how to do both or --

19 MR. LASH: We have had personnel licensed
20 on both units. For example, Pete Sena who will follow
21 me was licensed on both Unit 1 and Unit 2.

22 CHAIRMAN DENNING: But any particular time
23 they're dedicated towards one or the other?

24 MR. LASH: Predominately the SROs are
25 qualified and maintain a license, an active license,

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1 only on a single unit.

2 CHAIRMAN DENNING: Thanks.

3 MR. LASH: A time line of Beaver Valley.
4 This is a recent time line starting in 1998. The
5 first item I'd point out there is that FirstEnergy
6 Nuclear Operating Company was formed in December of
7 1998. And that operating company has now matured to a
8 fleet organization and is staffed to support all
9 functional areas at the three nuclear stations Beaver
10 Valley, Davis-Besse and Perry.

11 FENOC Corporate is currently charged with
12 providing governance and oversight of all station
13 activities.

14 Beaver Valley was purchased by FirstEnergy
15 from Duquesne Light & Power Company in late 1999
16 through an asset swap of fossil fire units for the
17 nuclear station.

18 In early 2000 FENOC implemented a full
19 potential program for Unit 1 and Unit 2 with a key
20 objective of managing design margins and increasing
21 the electrical output of both units. The EPU project,
22 which is a subset of this potential program, has
23 updated the station's analyses to include the selected
24 final design of the Unit 1 steam generators, which
25 were already referenced as the Model 54, which were

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1 recently installed during the last outage at Unit 1.
2 We'll talk about that briefly in a moment.

3 In total, the EPU project and its
4 supporting projects, steam generator replacement,
5 containment conversion, best estimate LOCA and others
6 that will be referred to this morning span a period of
7 6 years. As a result of the project, Unit 1 and Unit
8 2 have established a revised baseline of supporting
9 plant analyses that will be used to manage design
10 margins for the remaining life of both units. This is
11 in keeping with the original premises of the parent
12 full potential program that I spoke of earlier.

13 I previously mentioned the recently
14 completed outage at Unit 1. Let me briefly touch on
15 the scope and significant accomplishments of that
16 outage.

17 This is a picture of our containment. You
18 can see that we replaced all three steam generators in
19 this outage. By the way, this outage completed April
20 19, last Wednesday at 2018. And Unit 1 has achieved
21 100 percent power, full power operation on Sunday at
22 1400 hours and it remains at 100 percent power.

23 So during the outage we replaced the steam
24 generators and the reactor vessel head with a modified
25 simplified design, and the major accomplishments in

1 these replacements is obviously the elimination of the
2 Alloy 600 aspect of materials that were associated
3 with the older components.

4 Now shown here, because it's not in
5 containment, is the main unit generator rotor was
6 replaced. It has a short. We replaced it. And the
7 main unit generator itself was rewound.

8 Now there were many other activities, but
9 I won't go through all of those.

10 I would point out that the average time
11 frame to do a steam generator outage first time for a
12 station is about 82 days. Beaver Valley accomplished
13 this outage in 65 days. And I believe that to be a
14 very positive indication of both the strength of the
15 organization as well as the level of planning and the
16 preparedness for that outage.

17 The larger power uprate which we're
18 referred to and why we're here today, 8 percent was
19 initiated in mid-2000 and used an initial scoping
20 phase to determine the best approach and the optimum
21 targeted licensed power level. As a result of the
22 scoping evaluation, a target power level of 2900
23 megawatts thermal or 2910 megawatts thermal NSSS was
24 selected.

25 As you can see, that target aligns us very

1 well with our peer three loop Westinghouse units that
2 have already previous uprated. We benchmarked closely
3 these units, both their approach to uprate and their
4 operating history since its implementation. We feel
5 that collectively using the experience of these
6 stations gives us confidence in the approach we have
7 chosen. Specific examples of benchmarking in
8 implementation would be the use, for example, of the
9 specification for Model 54 steam generators used at
10 Farley Station and now at Beaver Valley. And the
11 phased approach to implementing the uprate, which we
12 will be discussing in greater detail later on in the
13 presentation.

14 MR. CARUSO: Have you ever considered
15 doing the stretch uprate?

16 MR. LASH: No, we have.

17 MR. CARUSO: I mean, I don't know if
18 you've ever --

19 MR. LASH: We've never discussed it.

20 MR. CARUSO: Never discussed that?

21 MR. LASH: Next slide, please.

22 In the area of oversight, executive and
23 senior management oversight of the project has been in
24 place since its inception. The site leadership team
25 has been closely involved, and this team includes the

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1 site Vice President, myself, the Plant Manager and
2 Engineering Director.

3 A FENOC executive leadership team has also
4 provided oversight and this includes our Senior Vice
5 President of Engineering currently Dan Pace who bring
6 unique experience in operating activities from his
7 previous role at Entergy.

8 Oversight of the engineering and licensing
9 process that supports this uprate has been directly
10 performed through implementation of the mentioned
11 boards, committees and assessments. And an example of
12 the independent assessment you find at the bottom
13 there would be the NPR Associates for a review of our
14 uprate supplemental.

15 That completes my introductory comments.
16 And if there are no other questions, I will turn over
17 the presentation to Pete Sena, the Director of
18 Engineer for Beaver Valley. Thank you.

19 MR. SENA: Good morning. Again, I'm Pete
20 Sena. I am the Director of Engineering at Beaver
21 Valley. My previous position at Beaver Valley was as
22 the Operations Manager and also as a senior reactor
23 operator at both units. So I did hold a senior reactor
24 operator license, active license for both units
25 simultaneous. So I'd take a stand working both units

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1 one at a time, so I do have a unique perspective as
2 far as the differences between the two units. And
3 when we come into questions with respect to some of
4 those specifics during the presentation, I can speak
5 to it. And also we have one of our shift managers
6 here, George Storlis, who is also licensed in both
7 units, however at a different times. So we will be
8 able to provide the Chairman with additional detail as
9 you request.

10 I will speak to principally the
11 preparations for the uprate, the general criteria, the
12 project team and the technical reviews. And before I
13 do so, I do want to comment that we at Beaver Valley
14 did attend the previous Subcommittee meeting that
15 Ginna participated in. We found that to be extremely
16 helpful as we prepared for our presentation, and we
17 have tailored our presentation we believe to what the
18 Committee desires. We will focus heavily on our
19 safety analysis so you can understand the margins that
20 remain following the uprate. We will be going into
21 great detail on our LOCA and our limiting non-LOCA
22 transients, such as a loss of feedwater and
23 uncontrolled rod withdrawal accident. So as we go into
24 those details, I think you'll appreciate what margins
25 do remain.

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1 All right. As you can see from this next
2 slide there were several amendments that have prepared
3 Beaver Valley for the power uprate. And again, the
4 uprate project was a full potential project initiated
5 back in the year 2000. Just that some of these
6 amendments will be touched on as we go through the
7 presentation, but I would like to speak to several of
8 them right here.

9 The positive moderator temperature
10 coefficient was previously approved and implemented
11 back in the year 2002. So what that has enabled us to
12 do is to gain operating experience on startup with a
13 slightly positive MTC throughout the years now that
14 we've had several cycles of operation. I personally
15 was the first SRO to perform a reactor startup with
16 that slightly positive MTC. Now that experience and
17 the lessons learned have been captured and formalized
18 for subsequent crews and subsequent startups.

19 Also the alternate source term, we will speak
20 about that again in the future, but we did selectively
21 apply AST to several accidents such as a fuel handling
22 accident LOCA, rod ejection. And what this permitted
23 Beaver Valley to do was to eliminate or retire circle
24 systems, and one in particular would be what's called
25 the control room air model pressurization system

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1 which, Mr. Sieber, you may remember that that has
2 challenged the plant in the past with an inadvertent
3 actuation which had resulted in a dual unit shutdown,
4 a tech spec 303 shutdown. So there were several
5 benefits towards that selected implementation.

6 Finally, containment conversion and best
7 estimate LOCA, those amendments were previously
8 approved by the NRC in the first quarter of this year.
9 On the containment conversion, there is an industrial
10 safety benefit that the site has realized with respect
11 to more frequent and safer containment entries at
12 power to allow for inspection of various components as
13 we see fit.

14 CHAIRMAN DENNING: What did you lose on
15 that in terms of -- you know, it's never been
16 absolutely clear to me why they were sub-atmospheric
17 and what the perceived benefits were of that and how
18 this might impact it.

19 MR. SENA: What I'd like to do is defer
20 that because we have an entire presentation on the
21 containment conversion and we're going to go through
22 that in great detail.

23 CHAIRMAN DENNING: Okay.

24 MR. SENA: A couple of things, though. We
25 did not change the containment design pressure of 45

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1 pounds. We did not change the structural design
2 temperature of 280 pounds. But there are several
3 aspects that were a benefit to the plant. For
4 example, the increased initial pressure provides
5 additional back pressure for the loss of coolant
6 accident. However, but we still need to meet our
7 designed pressure of 45 pounds. So we will go into the
8 detail on that particular amendment.

9 MEMBER SIEBER: Maybe before you soot away
10 from that, the idea early on was to be able to build
11 a smaller containment, spend less money on concrete
12 and rebar. And if you started out at a sub-
13 atmospheric pressure, the presumption was that you
14 would not reach as high in ultimate pressure. On the
15 other hand, the containment was built as a large dry
16 strong containment and the sub-atmospheric really
17 didn't change things all that much.

18 One of the advantageous, though, is you
19 get increased head to the sump because you're starting
20 at higher pressure, which could assist in the
21 recirculation phase of a LOCA accident.

22 I have a question about the positive
23 moderator temperature coefficient. It's quite common
24 to have a positive moderator temperature coefficient
25 when the plant is cold. I presume that you're still

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1 positive when the plant is hot early in core life?

2 MR. SENA: It's --

3 MEMBER SIEBER: And that goes away
4 sometime probably a third of the way through core
5 life?

6 MR. SENA: At about 30 percent power.
7 We're really starting off with zero feedback, around
8 a zero moderator temperature coefficient upon initial
9 criticality and the initial power ascension. Once you
10 come up to around 30 percent power and increase power,
11 it then starts --

12 MEMBER SIEBER: It goes the other way?

13 MR. SENA: -- inching it in the positive
14 direction.

15 MEMBER SIEBER: Oh, okay. And does that
16 stay throughout the life of the cycle?

17 MR. SENA: Well, again throughout the
18 cycle the same. As --

19 MEMBER SIEBER: At burndown it changes?

20 MR. SENA: -- you bring up the boron --
21 right. Then you're progressing towards a more
22 traditional negative MTC.

23 MEMBER SIEBER: Right.

24 MR. SENA: To maybe minus 4 or minus 5.

25 DR. BANERJEE: The increased pressure,

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1 does that lead to increased temperature in the sump
2 water?

3 MR. SENA: I'll tell you what we're going
4 to do is we're going to go through specifically the
5 need for containment overpressure during our
6 presentation.

7 DR. BANERJEE: Right.

8 MR. SENA: We currently at Unit 1 do
9 credit containment overpressure and will continue to
10 credit overpressure. And the onset of the accident,
11 Mike, what's our initial steam temperature about 280
12 degrees?

13 MR. TESTA: This is Mike Testa, the
14 Project Manager at Beaver Valley.

15 Pardon, could you repeat?

16 MR. SENA: The initial temperature for the
17 assumptions for containment overpressure, for
18 containment sump temperature?

19 MR. FREDERICK: You want to answer. I'm
20 here. This is Ken Frederick.

21 When the initial pumps start, the sump
22 temperature is around 260 degrees.

23 DR. BANERJEE: And what would have been in
24 the sub-atmospheric case?

25 MR. FREDERICK: It's roughly the same.

1 I'll show you some slides later that show you how that
2 changes.

3 DR. BANERJEE: So you say it doesn't
4 change?

5 MR. FREDERICK: It goes up a few degrees,
6 not much. The initial pressure change does not really
7 impact the transient conditions and some of that's due
8 to some methodology changes that we've incorporated in
9 its analysis.

10 DR. BANERJEE: Okay. You'll speak of this
11 in detail, right?

12 MR. FREDERICK: Yes.

13 MR. SENA: Yes. We have a specific
14 presentation talking specifically towards containment
15 over pressure.

16 Finally on the best estimate LOCA again,
17 that was recently approved. Both containment and
18 conversion and best estimate LOCA were both approved
19 first quarter of this year and have been implemented
20 at Unit 1 upon the completion of the Unit 1 outage.

21 At Unit 2 we have a full outage, those two
22 amendments will be implemented on the completion of
23 the Unit 2 outage.

24 CHAIRMAN DENNING: Was that essentially to
25 be able to accommodate the uprate?

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1 MR. SENA: Yes, it was.

2 All right. The best estimate LOCA that
3 we're speaking of is not the ASTRUM methodology
4 utilized by Ginna, but the more traditional
5 COBRA/TRAC. And we will discussing best estimate LOCA
6 in a future presentation. But it is the same
7 methodology used by Gravewood, Byron.

8 Next slide, please.

9 Again, is the key elements of the uprate.
10 I think I've spoken to these already with respect to
11 the containment conversion and best estimate LOCA.
12 And, again, we will go into great detail on analyses.

13 Next slide.

14 And the message about this slide is simply
15 that we at Beaver Valley did not forge new ground
16 here. We followed the same methodology used by other
17 utilities in their uprate. There are no new or
18 unlicensed industry methodologies being applied here.

19 Next slide.

20 As Mr. Lash said, this was a Beaver Valley
21 led project. The ownership remained with us at the
22 site. We did have corporate oversight, corporate
23 oversight and governance. But, again, the ownership
24 remained with our experienced site personnel.

25 We provided overall project management and

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1 direction. But, again, we had significant support from
2 our teammates, from Westinghouse and Stone & Webster.
3 And, again, many are here today in support and are
4 various subject matter experts that we may call upon
5 throughout the presentation.

6 Next slide.

7 Again, we at Beaver Valley, even though we
8 did have vendor support, we reviewed and approved the
9 design inputs and performed detailed owner acceptance
10 of each vendor calculation.

11 Finally, I do want to make a comment in
12 recognition of the NRC Staff. The NRC review and
13 challenges and various RAIs were very detailed, very
14 challenging and did result in a better project here
15 today. And in particular, the Staff audits that were
16 performed either at Westinghouse or at Beaver Valley
17 in the area of PSA, safety analysis and radiological
18 assessment did significantly help us to come to
19 closure on many open items and also significantly
20 streamlined the review process. So we do appreciate
21 that from the NRC.

22 Next I'd like to introduce Mark Manoleras.
23 Mark is the Manager of Design Engineering at Beaver
24 Valley. Mark will be looking at the plant
25 modifications that we had done and plan to do at

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1 Beaver Valley.

2 Thank you.

3 MR. MANOLERAS: Thank you, Pete.

4 My name is Mark Manoleras. I'm the Design
5 Engineering Manager at Beaver Valley. I've been the
6 Design Engineering Manager since 2002. My
7 department's responsibility has been the oversight and
8 performance of the modification packages and the
9 safety analysis associated with the uprate.

10 At this time I'd also like to mention in
11 the back, Mahesh Patel. Mahesh Patel is my lead
12 electrical engineer. He will be here to support the
13 second part of my presentation.

14 Next slide, please.

15 I'd like to discuss three areas today.
16 I'd like to discuss the plant modifications that were
17 performed to support the safety analysis for the power
18 uprate. Many of these modification packages were
19 performed to satisfy initial conditions in the safety
20 analysis. I will touch on the modification package,
21 discuss it briefly and we will discuss each
22 modification in great detail when we come up to the
23 safety analysis section.

24 I'd also like to spend a few minutes to
25 talk about the electrical system summary. The

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1 electrical system summary we will spend some time on
2 it. There was very minor changes associated with the
3 electrical system associated with the power uprate.
4 So we will touch on it in my portion of the
5 presentation.

6 And we will also discuss the use of
7 operating experience. The operating experience that
8 we touched on during the project.

9 Next slide, please.

10 As you see, this is the start of a list of
11 our plant modifications that were performed for the
12 power uprate. I will discuss each modification and
13 then I will identify its status whether it had been
14 implemented at Unit 1 or Unit 2.

15 The first modification is replacement of
16 our charging/safety injection pump rotating
17 assemblies. This modification extends our pump runout
18 flow limit and it improves high head margin and it
19 improves small break LOCA margin.

20 At Unit 1 we have replaced all three of
21 our charging pumps. At Unit 2 we have currently
22 replaced two of those three pumps, and currently are
23 planning to replace our third pump prior to our Unit
24 2 outage, which will implement some of the amendments
25 that you saw previously.

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1 The next modification package I would like
2 to discuss is the addition of fast acting feedwater
3 isolation valves at Unit 1. These valves reduce
4 containment pressure following a mainstream line break
5 inside containment. And they also provide redundant
6 isolation capability for feedwater isolation events.
7 These feedwater isolation valves are already existing
8 at Unit 2.

9 I'd also like to discuss briefly the
10 addition of aux feed cavitating venturies at Unit 1.
11 These venturies minimize mass input to containment and
12 reduce aux feed flow on a feedline break and maintain
13 minimum flow to the intact steam generator. These
14 cavitating venturies already exist at Unit 2.

15 We also added a reactor cavity drainage
16 port at Unit 1 to facilitate post-accident drain to
17 improve NPSH performances as pump draw from the sump.
18 We intend to install that reactor cavity drainage port
19 at Unit 2 in our next outage.

20 We eliminated our quench spray cutback
21 feature and it's not longer required due to the
22 containment analysis at Unit 1. This quench spray
23 cutback does not exist at Unit 2.

24 Additionally, we replaced our steam
25 generators at Unit 1 and that includes the narrow

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1 range level transmitters. We increased the narrow
2 range span. And we'll talk about that in great detail
3 in the non-LOCA analyses that follow.

4 DR. BANERJEE: Why was it necessary to put
5 those auxiliary cavitating venturies?

6 MR. MANOLERAS: Yes. What we did that for
7 was we wanted to make sure that we minimized the mass
8 input to containment following that feedline break. We
9 wanted to do that. Basically reduce the mass addition
10 to the containment following a feedline break.

11 DR. BANERJEE: And that came about because
12 of the uprate?

13 MR. MANOLERAS: That's correct. Basically
14 part of the containment analyses.

15 MR. TESTA: Yes. This is Mike Testa again
16 from Beaver Valley.

17 As Mark said, Unit 2 plant already had
18 that feature, had cavitating venturies installed in
19 the auxiliary feedwater system.

20 When we looked at Unit 1 we wanted to
21 again, as Mark said, help support the revised mass and
22 energy release to the containment for feedline break
23 and a steamline break. And it also helps to protect
24 the pumps from run off condition. So early on in the
25 project we decided to install those cavitating

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1 ventures and then credit those in the mass and energy
2 release for the containment analysis.

3 DR. BANERJEE: I guess a more general
4 comment is I see a list of things you're doing, but I
5 don't have a clear picture of why you do them. And
6 does this come out later on or --

7 MR. MANOLERAS: Yes. Actually, when we
8 get to the safety analysis section of the presentation
9 we will identify which modification packages satisfy
10 which initial conditions of those analyses.

11 DR. BANERJEE: Anyway, if you could just
12 briefly mention the why, that would be very helpful.

13 MR. MANOLERAS: Okay. I will do that.

14 DR. BANERJEE: Why do you replace the
15 steam generator? Maybe it's obvious, but we'd like to
16 know.

17 MR. MANOLERAS: Yes. For example, our
18 Unit 1 steam generators were the oldest steam
19 generators in the country. We basically had very
20 limited tube plugging margin there. So we installed
21 new steam generators. The generators that we
22 installed actually do not have any tubes plugged. So,
23 obviously, that was the reason that we did that Unit
24 1. That's an example.

25 DR. BANERJEE: Okay.

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1 MR. MANOLERAS: Okay. Next slide, please.

2 We replaced our high pressure turbine at
3 Unit 1 with a turbine with all reaction design. At
4 Unit 2 we're going to do that also. We basically
5 needed to do that to basically maximize our megawatt
6 capacity; that's why we did that.

7 At Unit 1 we already installed stakes in
8 our main condenser to eliminate any vibration issues.
9 We intend to install those stakes in the Unit 2
10 condenser so we do not have any flow induced vibration
11 issues there.

12 MEMBER SIEBER: What's the tube material
13 at Unit 2 condenser.

14 MR. TESTA: It's stainless.

15 MEMBER SIEBER: Stainless. Yes. Is the
16 original.

17 MR. TESTA: Yes.

18 DR. BANERJEE: And the steam generator
19 tubes?

20 MR. TESTA: Steam generator tubes?

21 MEMBER SIEBER: 690 for Unit 1, 600 for
22 Unit 2

23 MR. MANOLERAS: 600. And we go into great
24 detail. We have a materials presentation. We'll go
25 into great detail on that.

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1 At Unit 1 we did not have to replace our
2 cooling tower fill. We had adequate cooling tower
3 fill. We did not have to replace that.

4 At Unit 2 we put in a high efficiency
5 fill.

6 MEMBER SIEBER: You may want to tell what
7 cooling tower fill is.

8 MR. MANOLERAS: Basically this is the
9 material in the cooling tower that helps I guess the
10 heat exchange capacity or capability of that cooling
11 tower. So the fill material will allow the
12 dissipation of heat in the cooling tower, I guess is
13 the best way to describe it.

14 DR. BANERJEE: Why does it do that?

15 MR. TESTA: Again, this is Mike Testa.

16 For the cooling tower on the circ water
17 side of the cooling tower, basically you pump the
18 water into the tower and the water will rain down,
19 basically, in effect over this fill. And the fill it
20 helps to aerate, in effect break up the water and help
21 aerate it. That way when you bring the natural draft
22 of the tower through it, it'll help remove heat.

23 MEMBER SIEBER: In Unit 1 it looks like
24 venetian blinds.

25 DR. BANERJEE: Huh?

1 MEMBER SIEBER: In Unit 1 it looks like
2 venetian blinds and the water cascades down through it
3 and the air is going through at right angles.

4 I take it that all the asbestos that was
5 in there is now gone?

6 MR. MANOLERAS: That's correct.

7 DR. BANERJEE: Then the last point raise
8 set pressure, is that just for the cycle or what?

9 MR. MANOLERAS: No. We intend to make a
10 permanent change. We've actually made that change. We
11 raised that setpoint to the MSR reheater relief
12 valves. We did some analyses, BOP analyses that
13 identified that we would have limited margin error. So
14 we went out and we retested and reset our MSR relief
15 valve setpoints.

16 DR. BANERJEE: Margin to what?

17 MR. TESTA: This is Mike Testa again.

18 As Mark said, we redid the heat balance
19 for the power uprate and we looked at the operating
20 pressure at the MSR. The operating pressure in effect
21 went up about 10 pounds. Okay. We had relief valves
22 that were set originally at 250 psig. And then
23 because of the uprate and they increased in operating
24 pressure of about 10 pounds, we modified the relief
25 valves to relieve at 260. So in other words, the

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1 operating pressure went up 10 pounds. We raised the
2 set pressure 10 pounds.

3 MEMBER SIEBER: So you're still way under
4 the design pressure?

5 MR. TESTA: Yes. Yes. Yes.

6 DR. BANERJEE: Do these relief valves
7 latch open or do they close as the power goes back and
8 forth, the pressure?

9 MR. TESTA: They basically have a set
10 pressure. They will pop at that set pressure.

11 DR. BANERJEE: Right. And then--

12 MR. TESTA: And then they'll release and
13 then reset.

14 DR. BANERJEE: At some other pressure?

15 MEMBER SIEBER: Will, you blow down for
16 probably 5 percent.

17 MR. TESTA: Yes.

18 MEMBER SIEBER: It will close and then if
19 the pressure goes up again, it'll open again at the
20 original set pressure.

21 DR. BANERJEE: It doesn't factor?

22 MR. TESTA: No, does not.

23 MEMBER SIEBER: Hopefully.

24 MR. TESTA: Again, we've already done
25 this. We have operating experience on Unit 2 in the

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1 past spring outage. We've already done that
2 modification. And we've had no issues, no problems
3 with that.

4 MEMBER SIEBER: The pressure is not high
5 and there's a lot of volume there, so --

6 MR. TESTA: Yes.

7 MEMBER SIEBER: -- it shouldn't change.

8 MR. MANOLERAS: The next slide, please.

9 We increased the CD of our main feedwater
10 control valves. At Unit 1 we replaced the control
11 valve trim. At Unit 2 we are replacing the feed reg
12 valves. We did that basically to improve their
13 operating range and also to help stabilize our steam
14 general level control.

15 MEMBER SIEBER: What kind of trim did you
16 put in Unit 1 feed reg valves? It originally had what
17 they called the hush trim, which was about the third
18 mod.

19 MR. TESTA: This is Mike Testa.

20 We put in hush trims on Unit 1.

21 MEMBER SIEBER: That's what was in there.

22 MR. HANLEY: This is Norm Hanley from
23 Stone & Webster. Repeat your question, please

24 MEMBER SIEBER: Ten or 15 years ago it had
25 hush trim in it and there was a lot of problems with

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1 the valve on ability to control the low flows. The
2 valve was modified several times, all three of them
3 were. I'm wondering what you did recently?

4 MR. HANLEY: The recent change really
5 didn't modify the trims that you have in there now.
6 It just increased the CV. The operating experience
7 with the latest set of trims was well. So we didn't go
8 into a redesign of the trim. It was just get us more
9 CV so we'd get a better operating range.

10 DR. BANERJEE: Well, how did you get a
11 better CV?

12 MR. HANLEY: Yes. We went back to the
13 vendor. The original valves, I think, had a large of
14 CV, about 1100. And right now we've got 1050 in
15 there. So the valve could accommodate. So the vendor
16 designed the CV to give us 1050 maximum and allowed us
17 a good operating range during the power uprate. The
18 values should operate between 75 and 80 percent open
19 during the uprate.

20 MEMBER SIEBER: It seems to me the way
21 that the plant was originally built those valves were
22 throttled quite a bit. Since it has electric feed
23 pumps instead of turbine drive feed pumps, turbine
24 driven feed pumps have basically a constant
25 differential across the reg valve. With electric

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1 pumps at low loads there's a big pressure drop there.
2 It's very hard on the valves; that's why the valves
3 were modified several times to try to tone down the
4 energy dissipation. After the hush trim was
5 installed, that was pretty much the end of the feed
6 reg valve problem.

7 MR. HANLEY: In fact, we just installed
8 them in Unit 1 and we did a start up and the valve
9 behaved very well during start up.

10 CHAIRMAN DENNING: Be sure to speak into
11 the mike.

12 MR. HANLEY: All right.

13 MR. SENA: This is Pete Sena.

14 Just one item, Mr. Sieber, that the
15 operating crew from this last start up at Unit 1 did
16 comment that the feed reg valve control was the best
17 they had seen at low power operations for start up.
18 There were no anomalies.

19 MR. MANOLERAS: Okay. Jim had already
20 discussed the replacement of the rotor and the rewind
21 of the starter.

22 We additionally modified our heater drain
23 control valves at both units to increase operating
24 range and improve capacity. And we replaced our
25 instrument replacements for main steam and feedwater

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1 flow for the higher flow ranges that we'll discuss
2 later in the safety analysis presentation.

3 CHAIRMAN DENNING: Before you move on to
4 that, I do have a little digression. And that is
5 regards to sump blockage. At some point, I presume in
6 the near future, you're going to be making changes or
7 can you tell us what the status is of that?

8 MR. MANOLERAS: Sure.

9 CHAIRMAN DENNING: And what the character
10 of the changes will be and when they'll occur.

11 MR. MANOLERAS: Sure. We currently have
12 about 120 square foot sumps. We're going to be
13 expanding those sumps by a factor of at least 10. We
14 are going to put much larger passage strainers in at
15 Unit 1 and Unit 2. We intend to install the passive
16 strainer system at Unit 1 in the upcoming outage and
17 at Unit 1 in our next outage. We will also install
18 that passage system at Unit 1.

19 We are currently doing the analysis
20 associated with the strainer design, putting them in
21 the actual mix of the insulation and boric acid, the
22 mix, doing the testing of our strainer design to make
23 sure that all the assumptions that we put into the
24 analysis are put as far as DP across the strainers and
25 whatnot. So we're going right down the path of the

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1 GSI-191 requirements.

2 CHAIRMAN DENNING: So the change for Unit
3 2 it will occur prior to the power uprate, is that
4 true?

5 MR. MANOLERAS: It's going to be installed
6 in our next outage, the physical modifications to the
7 sump, which our next outage is when we intend to begin
8 our escalation and our power uprate.

9 CHAIRMAN DENNING: Whereas in Unit 1, of
10 course, it would follow?

11 MR. MANOLERAS: Unit 1 we intend to
12 perform a mid-cycle uprate and our next refueling
13 outage before we went to the full power uprate, we
14 would have the new sump in.

15 CHAIRMAN DENNING: Yes. And what kind of
16 thermal insulation do you currently have?

17 MR. MANOLERAS: We have several types of
18 thermal insulation. We have a metal-reflective. The
19 majority of our containment we do have metal-
20 reflective. We also have a material it's called, it's
21 abbreviated name is CALSIL. It's a material that is
22 like a plaster of Paris type of material that
23 encapsulated with --

24 CHAIRMAN DENNING: We're familiar with it.

25 MR. MANOLERAS: Okay. So we have some of

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1 that.

2 And we have several other types of
3 insulation also.

4 DR. BANERJEE: Do you have NUKON?

5 MR. MANOLERAS: Pardon me?

6 DR. BANERJEE: NUKON?

7 MR. MANOLERAS: NUKON? That's a term that
8 I am not familiar with. So I don't want to say that
9 we don't, but it's not a prevalent use of material in
10 our containment.

11 CHAIRMAN DENNING: You don't have a
12 fiberglass?

13 MR. MANOLERAS: Fiberglass?

14 CHAIRMAN DENNING: Fiberglass? Fiberglass
15 mats in any places.

16 DR. BANERJEE: Fibrous material?

17 MEMBER SIEBER: Yes, they're like blankets

18 MR. MANOLERAS: Yes. We don't have
19 significant quantities of any fibrous material. We
20 would have very limited fibrous material, maybe in an
21 application like around a loop stop valve where we
22 would have -- and I'm talking very, very small
23 quantities of that where we would have some space
24 limitations. Like we would pack it in around a valve,
25 but it would be in very small quantities. And what

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1 we're going to do is in each refueling outage we're
2 going target and take a hard look at that material to
3 see if we can get it out of there and replace with
4 metal reflective.

5 DR. BANERJEE: What are you insulating
6 your steam generators with?

7 MR. MANOLERAS: The replacement steam
8 generators? We replaced the CALSIL associated with
9 those steam generators and put metal reflective in
10 during this last outage in every area that we could.

11 DR. BANERJEE: All the new steam
12 generators will have metal reflective?

13 MR. MANOLERAS: That's correct.

14 MEMBER SIEBER: Unit 1.

15 MR. MANOLERAS: In Unit 1

16 CHAIRMAN DENNING: At Unit 1.

17 MR. MANOLERAS: When we replaced our steam
18 generators -- to make sure we're very clear. At Unit
19 1 when we replaced our steam generators we put in
20 metal reflective insulation and we took out those
21 materials that have been identified in that GSI-191.

22 CHAIRMAN DENNING: Will there be a future
23 replacement of steam generators at Unit 2 or how much
24 margin do you still have there?

25 MR. MANOLERAS: We have significant tube

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1 plugging margin at Unit 2. I'm sure that in our long
2 range plan that's something that we'll look at. But at
3 the present time we have not targeted that
4 replacement. We have significant margin at Unit 2.

5 CHAIRMAN DENNING: And plant life
6 extension is still to come?

7 MR. MANOLERAS: That's correct. We are
8 currently working on what we term to be a license
9 renewal submittal.

10 DR. BANERJEE: How do you control pH?

11 MR. MANOLERAS: Our chemical addition
12 system we currently use an additive. It's sodium
13 hydroxide, NaOH.

14 DR. BANERJEE: Do you have any aluminum in
15 the containment?

16 MR. MANOLERAS: Yes, we do. We keep track.
17 We have a very detailed program to keep track of
18 aluminum in containment so that we don't have, for
19 example, hydrogen generation is always a big concern.
20 So we have a very detailed program to keep track of
21 any aluminum that we place in containment. We have
22 very small quantities of aluminum in containment. We
23 know where it's at.

24 DR. BANERJEE: Well, will you address
25 these issue related to the sump and the change from

1 sub-atmospheric to atmospheric pressure and all that
2 sort of thing? Is there going to be a talk on this
3 sometime?

4 MR. MANOLERAS: You know, there's actually
5 a very detailed presentation that we've put in on the
6 containment conversion submittal.

7 DR. BANERJEE: And will it be done,
8 something?

9 MR. MANOLERAS: It will be done this
10 morning, I believe, or early in the afternoon. And I
11 believe we actually brought a slide to show our
12 conceptual design for our new sump strainer. We
13 actually have a picture of our sump strainer that we
14 are currently designing.

15 MEMBER SIEBER: But the conversion of the
16 containment to an atmospheric containment is already
17 approved and implemented?

18 MR. MANOLERAS: That's correct. That
19 license amendment has been approved and it has been
20 implemented at Unit 1.

21 MEMBER SIEBER: Okay. Before you jump
22 into the electrical system, when I was reading through
23 the application in the SER, particularly the marked-up
24 tech specs, I stumbled across a place where you are
25 eliminating the negative rate trip?

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1 MR. MANOLERAS: That's correct.

2 MEMBER SIEBER: What's that have to do
3 with EPU or anything else, or did you figure that was
4 just a good chance to get rid of something you didn't
5 like?

6 MR. MANOLERAS: Well, you hit right on the
7 head. The negative rate trip was not used in our
8 plant safety analysis. Additionally, there was an
9 owners group program to eliminate that trip. We took
10 this opportunity to implement that. That will reduce
11 surveillance burden for us at the station.

12 MEMBER SIEBER: Yes. The reason why it was
13 in there originally, though, was in case you dropped
14 a rod that the plant would trip before you started
15 operating with a big imbalance in the core. There was
16 a reason to do that. Did you change your operating
17 procedures to tell the reactor operator to trip the
18 plant when it gets to that condition?

19 MR. DURKOSH: This is Don Durkosh from
20 Operations.

21 Yes, we have immediate operator actions
22 for any dropped rod.

23 MEMBER SIEBER: Okay.

24 MR. DURKOSH: If we have more than one
25 dropped rod, we immediately trip the reactor.

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1 MEMBER SIEBER: More than one?

2 MR. DURKOSH: More than one, that's
3 correct. More than one.

4 MEMBER SIEBER: So what kind of offset do
5 you get if you just drop one rod all the way in in a
6 critical area, do you know? Has anybody done those
7 calculations? That's why we had the trip so you
8 wouldn't have to do the calculation.

9 MR. MURTAGH: This is Brian Murtagh from
10 Design Engineering.

11 The Westinghouse WCAP that evaluated the
12 elimination of the negative rate trip essentially,
13 from what I remember, it was if you evaluated the most
14 reactive rod worth and that were to trip, you would
15 still not be tripping on negative rate. So because we
16 do not credit that in the safety analysis, that's why
17 it was eliminated.

18 MEMBER SIEBER: Okay. But that's
19 different for every cycle. The Westinghouse WCAP was
20 done for the envelop of cores that you could design
21 and could put into that kind of a plan. I take it
22 during the reload safety evaluation that's analyzed
23 again?

24 MR. PENKROT: This is Jack Penkrot from
25 Westinghouse.

1 We do evaluate the dropped rod.

2 MEMBER SIEBER: Okay.

3 MR. PENKROT: For all the values up to
4 1,000 pcm. Whenever the negative rate trip was
5 eliminated, we increased the span that we evaluated
6 from zero to 500 to zero to 1,000. We're able to show
7 that peaking factors are adequate to handle any
8 dropped rod.

9 MEMBER SIEBER: Do you know the number and
10 the date of the WCAP so I could read it?

11 MR. PENKROT: I don't have that
12 information.

13 MEMBER SIEBER: Well, could you get it?

14 MR. PENKROT: Oh, yes. Sure.

15 MEMBER MAYNARD: This trip has been
16 eliminated at a number of plants. In fact, for most
17 plants most rods, a single rod, wouldn't give you the
18 negative rate trip anyway. But you have procedures
19 for recovering that rod --

20 MEMBER SIEBER: Yes, I know.

21 MEMBER MAYNARD: -- that limit. You can't
22 just pull it right back out and go to operating. So
23 you do have an off normal procedure that controls the
24 recovery from that to keep you within your safety
25 analysis.

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1 MEMBER SIEBER: I'd still like to read the
2 WCAP.

3 I was just trying to figure why it was
4 stuck in with all this other stuff as opposed to
5 standing out there by itself because it really is not
6 related to EPU or the containment change or alternate
7 source term or anything else. It's just out there.

8 MR. MURTAGH: Mr. Sieber, this is Brian
9 Murtagh again.

10 I can certainly get you that WCAP, a copy
11 of the WCAP.

12 MEMBER SIEBER: Well, we probably have it.
13 If the Staff's approved it, it's here. All I need is
14 the number. It'll be in our file.

15 MR. MURTAGH: Okay. We'll do our best to
16 try to find that number.

17 MEMBER SIEBER: If you want to give it to
18 me, that's even better. You know, I'm in love with
19 paper. You know, I get tons of it every week.

20 CHAIRMAN DENNING: Thank you.

21 MR. MANOLERAS: Yes. I believe Chris --

22 MR. MCHUGH: Chris McHugh from
23 Westinghouse.

24 I have that number on my laptop. I'll
25 look it up and give it to you in a couple of minutes.

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1 MEMBER SIEBER: Thanks.

2 MR. MANOLERAS: Thank you, Chris.

3 Any further discussion before I move on to
4 electrical system?

5 We added the slide here to discuss the
6 electric system impacts, the actual system impacts
7 because of the power uprate were actually extremely
8 minimal. I brought Mahesh Patel, as I mentioned
9 before, in case any questions are beyond me and we'll
10 have Mahesh answer those.

11 Our initial electrical system design is
12 robust. We basically took a look at all of our
13 electrical components. We looked at our Unit 1
14 transformer. We did not have to do any upgrades to our
15 Unit 1 transformer.

16 Our Unit 2 transformer we had to upgrade
17 that cooling system. And we did upgrade that cooling
18 system. We have several cycles of operation now with
19 that transformer and that cooling system. And the
20 modification packages that we did make basically had
21 their intended results. So our cooling system for our
22 transfer has been upgraded.

23 Our isophased bus duct, one of the issues
24 is OE and the industry looked as isophased bus duct
25 temperatures. We went out and did extensive

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1 maintenance our bus duct cooling systems at both units
2 to make sure that the material condition of those
3 cooling systems -- material condition was there. We
4 did not require any modification packages to those
5 cooling systems.

6 We did install temperature indicators in
7 those cooling systems so that we can do operator
8 rounds and ensure that the bus duct cooling system
9 meets its performance.

10 We obviously have operating limits on our
11 grid voltage, which we did not have to change in
12 reactive loads to look at post-trip voltages on our
13 buses. We did not have to make any modifications to
14 any of those limits because of the uprate.

15 Our grid we did detailed grid stability
16 studies and Beaver Valley can both receive and accept
17 trips on the grid without any impact. And we did not
18 effect our 4-hour station blackout coping study
19 because of the uprate.

20 MEMBER SIEBER: In Unit 1 are you
21 replacing the main unit transformer or are you going
22 to use the one that's still there?

23 MR. MANOLERAS: We're going to use the
24 existing transformer.

25 MEMBER SIEBER: You know that that had

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1 faults in it a couple of times?

2 MR. MANOLERAS: We have had to replace
3 that transformer. We had an inadvertent spraydown of
4 that transformer several years ago and it was
5 replaced, as you remember.

6 MEMBER SIEBER: Well, the replacement
7 transformer, the internal impedance was such that it
8 represented an unusual condition on the grid. I
9 presume that you know that.

10 MR. MANOLERAS: Yes, we do.

11 MEMBER SIEBER: But it called into
12 question the breaker capacity if you had to trip that
13 transformer free from the grid interrupting capacity.

14 MR. MANOLERAS: Mahesh Patel.

15 MR. PATEL: Yes. This is Mahesh Patel.

16 When we had a fault on the original
17 transformer, we had it built with a little bit higher
18 than the previous transformer. And we evaluated the
19 breaker capacity and that reduce the fault coming from
20 the system. And that makes the breaker capacity. And
21 the newer transformer is rated is 1058 MBA at 65
22 degree temperature rise.

23 MEMBER SIEBER: Okay. Thank you.

24 MR. MANOLERAS: The next slide, please.

25 Yes. In this last slide I'd like to just

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1 go over some of the industry OE and things we looked
2 at. Each specific presenter will discuss the specific
3 OE in his area.

4 We looked at, obviously, vibration issues.
5 We talked about staking the condenser. We looked at
6 things like the turbine control system running with
7 valves wide opened. We looked at the isophase bus duct
8 cooling capacity and transformer cooling. And Jim
9 discussed earlier we installed the leading edge
10 technology -- the leading edge flow meter for
11 measurement uncertainties.

12 Each presenter will discuss OE in his
13 particular area.

14 If there are no additional questions, I
15 would like to introduce A.R. Burger, our fuels
16 analyst.

17 MR. BURGER: Thank you, Mark.

18 Good morning.

19 As Mark indicated, my name is A.R. Burger.
20 I'm currently the supervisor of core design and
21 physics support. And I'm responsible currently for
22 the design oversight for not only Beaver Valley, but
23 also the Perry and also Davis-Besse unit.

24 I have supporting person Jack Penkrot.
25 He's a Westinghouse core designer. He's done core

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1 design for both Beaver Valley units for quite a few
2 years.

3 To give you a little background, I started
4 out in '82 as a reactor engineer down at Beaver
5 Valley. Starts physics testing at Unit 2 and power
6 central testing. Moved on to the fuel procurement and
7 contract administration in the '90s. And '98 to 2004
8 I became the core design, reload design coordinator
9 for Beaver Valley interfacing with all the contract
10 administration in implementing the core designs. And
11 currently I'm in the supervisor position.

12 I've been involved in EPU since the
13 inception back in 2000 and so we've preparing in the
14 core design area for that.

15 What I'm going to touch upon is the fuel
16 design and the core design aspects.

17 This represents the current design that we
18 have Beaver Valley. It's called the robust fuel
19 assembly. It's the same array, 17 by 17 as the
20 previous, which was a Vantage 5H that we had prior to
21 the RSA. We maintained the enrichment, the geometric
22 fuel geometry, the cladding, the loading of the
23 uranium, axial blanket height; all that has remained
24 the same.

25 The changes with the RFA that we've put

1 in, we have six cycles operating history on the RFA.
2 We implemented back at Unit 1 starting with cycle 15
3 in 2001 and that Beaver Valley introduced in cycle 10
4 2002. We did that for several reasons, one being the
5 uprate coming. We saw that coming and so we wanted to
6 get in to look at the RFA design. There's
7 intermediate flow mixers on the top three spans. That
8 will give you GMD margin that we would implement to
9 give us for the uprate.

10 MEMBER SIEBER: You have to change the
11 pressure drop across the core?

12 MR. BURGER: Yes.

13 MEMBER SIEBER: By how much?

14 MR. BURGER: There was a couple of pounds
15 difference.

16 MEMBER SIEBER: That's pretty much.

17 MR. BURGER: And that's why you have a
18 transition core penalty in that time. We've now got
19 fuel, RFAs in the entire core so we have a whole core
20 of that. We don't have any transition penalty and
21 things like that going on.

22 MEMBER SIEBER: Well, you have flow
23 distribution problems when you have a mixed core.

24 MR. BURGER: Right.

25 MEMBER SIEBER: On the other hand it seems

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1 to me the core flow went up instead of down in your
2 list of parameters. And I would expect it would have
3 gone down with this kind of fuel by a little bit.

4 MR. BURGER: Well, they're going to go
5 into that in the safety valve section.

6 MEMBER SIEBER: The pressure drop across
7 the steam generators, the new steam generators, is
8 less, right? Is that true? Less than the Model 51s?
9 54 is less DP than Model 51, is that true?

10 MR. BURGER: Excuse me. Could you repeat
11 the question, please?

12 MEMBER SIEBER: Is the pressure drop
13 across the new steam generators, the Model 54, less
14 than the pressure drop across the old steam
15 generators, which is Model 51?

16 MR. HALL: Yes. This is Jeff Hall,
17 Westinghouse.

18 That's correct. The Unit 2 generators are
19 Model 51.

20 MEMBER SIEBER: So you end up with higher
21 DP across the core, lower DP across the steam
22 generators and an overall slight increase in flow for
23 the whole system?

24 MR. HALL: That's correct.

25 MEMBER SIEBER: Okay. You just moved the

1 DPs around? Okay. Thanks.

2 CHAIRMAN DENNING: But of course they
3 would be different for Unit 1 and Unit 2 then?

4 MEMBER SIEBER: Yes, they are right now
5 because they haven't replaced steam generators in Unit
6 2.

7 MEMBER MAYNARD: Well, you'll also be
8 operating at a little bit different RCS temperature,
9 won't you, for your uprated condition?

10 MEMBER SIEBER: Well, yes. And that comes
11 about because of the change in flow and the change in
12 materials and the change in surface.

13 MR. BURGER: You have the 576.2 plus or
14 minus a couple of degrees of where we're at currently
15 for the uprate.

16 MEMBER SIEBER: Right.

17 MR. BURGER: And they'll go into that in
18 the safety analysis section where we're targeting to
19 go for two and a half for each unit.

20 MEMBER SIEBER: And your hot leg trip is
21 what? 617, something like that? They would normally
22 be operating at about 610 or 611 on the hot leg?

23 MR. BURGER: On the hot leg, yes.

24 MEMBER SIEBER: Okay.

25 MR. FREDERICK: This is Ken Frederick.

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1 Yes, that's correct, Jack. We'll go over
2 that later in my slides.

3 MEMBER SIEBER: Well, it sounds like it's
4 the same as Ginna. Same core parameter set.

5 MR. FREDERICK: In terms of the
6 temperatures, yes, it's very similar.

7 DR. BANERJEE: Was there any DNB testing
8 done on a prototype bundle or something?

9 MR. BURGER: Yes, there were supposedly
10 tests done for the RFA by Westinghouse when they
11 originally came out with them in 2002 and 2001. The
12 RFA has actually been out in the industry for quite a
13 few years.

14 MEMBER SIEBER: Yes.

15 MR. BURGER: There's 33 plants operating
16 with the RFA fuel design.

17 DR. BANERJEE: What are these mixes like
18 that give you better performance?

19 MR. BURGER: They just provide extra flow
20 mixing --

21 DR. BANERJEE: What are these mixes?

22 MR. BURGER: They're just an extra grid
23 that's put between the upper grid span. You'll notice
24 they're a little bit thinner than the standard grid
25 and, again, they're must meant to get flow mixing into

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1 the assembly so that that's all they're there for.
2 They provide a little bit more structural integrity
3 for the assembly also, a little bit more stiffer
4 assembly.

5 MEMBER MAYNARD: They just have little
6 pads in them that kind of redirect flow and mix the
7 flow right?

8 MR. BURGER: Mix the flow right.

9 MEMBER SIEBER: In a mixed core there are
10 some grids that don't contact the adjacent fuel
11 assembly grid. So from the seismic standpoint it's
12 meaningless.

13 MR. BURGER: Yes. There is no impact on
14 the seismic parameters.

15 DR. BANERJEE: And these tests were done
16 in a flow loop they had with heaters?

17 MR. BURGER: That's right.

18 DR. BANERJEE: Electrical heaters?

19 MR. BURGER: I believe they were, yes. The
20 VIPRE loop that they use for Westinghouse.

21 MR. CARUSO: Yes.

22 MEMBER SIEBER: Yes.

23 MR. CARUSO: Westinghouse has a test loop
24 that they run down in Columbia.

25 MR. BURGER: VIPRE loop down there that

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1 they run.

2 MEMBER SIEBER: Yes. They've been doing
3 that for years.

4 What correlation are they on now? It used
5 to be --

6 MR. BURGER: We'll go into that. There's
7 a WRB-2M correlation that they'll be using for the RFA
8 and we'll be implementing that with the uprate. Right
9 now we're not utilizing it. But when we uprate, we'll
10 implement the WRB-2M. And, again, they'll go into
11 that in the safety analysis.

12 MEMBER SIEBER: And here you can't have a
13 mixed core to implement that correlation?

14 MR. BURGER: Right. We were going to
15 implement an older design, put it in there. We have to
16 go and use the other correlations which are still
17 applicable.

18 MEMBER SIEBER: Right.

19 MR. BURGER: When we originally did the
20 analysis back in 2000 we were going to have a mixed
21 core, but it's delayed enough that we now have a full
22 core of RFAs, so we won't need that.

23 MEMBER SIEBER: Well, you have to go to
24 the most conservative correlation that you have.

25 MR. BURGER: Right.

1 DR. BANERJEE: So the increased power is
2 accommodated by --

3 MR. BURGER: Why don't we go to the next
4 slide and that will show.

5 DR. BANERJEE: This increase in DNB?

6 MR. BURGER: We'll let into it, after this
7 one. This one will show you that the DNB margin and
8 we're going to use the WRB-2M correlation, as I
9 mentioned, for the IFMs being in there. The RFA also,
10 as I mentioned, provides a better grid design for
11 grid-to-rod fretting issues. Beaver Valley and the
12 industry had had issues with grid-to-rod fretting and
13 so we went to that RFA design early on for fuel
14 failures to get rid of those.

15 We also at that time, there was issues
16 with incomplete rod insertion in the industry. So the
17 RFA provides a slightly increased the I2 giving a
18 stiffer assembly and more margin --

19 MEMBER SIEBER: A larger diameter guide,
20 too?

21 MR. BURGER: Yes. The IB stayed the same
22 and the OD increased slightly.

23 MEMBER SIEBER: Okay. And I take the
24 grid-to-rod fretting you're using the -- you have two
25 dimples and two springs made out of Zircaloy. And

1 those springs as the become irradiated, they relax.

2 MR. BURGER: Right. Correct.

3 MEMBER SIEBER: To the point where they
4 aren't springs anymore?

5 MR. BURGER: Yes. They redesigned those
6 assemblies so they had more contact surface area with
7 the springs. And we have not had any grid-to-rod
8 fretting with those assemblies and we have three
9 cycles of operation. So they basically have gone
10 through a full lifetime of those.

11 MEMBER SIEBER: That wasn't really an
12 issue at that plant anyway.

13 MR. BURGER: What? At Beaver Valley?

14 MEMBER SIEBER: Yes.

15 MR. BURGER: Yes. We had grid-to-rod
16 fretting issues with the 5H, yes.

17 MEMBER SIEBER: Oh, okay.

18 MR. BURGER: Yes. We had fuel failures
19 associated with that.

20 DR. BANERJEE: But to get the increased
21 power out, does the surface area in contact with the
22 coolant increase or not?

23 MR. BURGER: No. We'll go to the next
24 slide. What we'll do is we did conceptual core designs
25 for the uprate conditions. We did that both with the

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1 Westinghouse codes, the ANC codes. We also run in-
2 house down at our offices. Basically to get the
3 increased power out we're going to go from equilibrium
4 to core cycles of 18,800, 20,200.

5 We have had cycles up above 20,200 just
6 because of the way the outages were scheduled. Beaver
7 Valley Unit 2 cycle 10 was 20,400. So we have had
8 cores where there's much energy as we'll be doing for
9 the uprates.

10 Basically your linear heat generation
11 rate's going to go up. So the fuels all stayed the
12 same on the surface area and everything else. Just
13 put --

14 DR. BANERJEE: So your heat flux goes up?

15 MR. BURGER: Right. And it's in the same
16 vein as the others that we mentioned earlier, kilowatt
17 p er foot is in that same range --

18 DR. BANERJEE: So what allows you to get
19 more heat out of the same surface area fuel?

20 MEMBER SIEBER: Higher temperature.

21 MR. BURGER: Higher temperature. Yes.

22 DR. BANERJEE: No, no. I mean from the
23 point of view of limits?

24 MR. BURGER: Our peaking factors will
25 remain the same.

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1 MEMBER SIEBER: You got closer to the
2 point of 200.

3 DR. BANERJEE: What?

4 MR. BURGER: The peaking factors were to
5 remain the same. What we did was to get more margin on
6 the fuel is we put in the IFM, so that gives DNB
7 margin and --

8 DR. BANERJEE: So you get your DNB margin
9 by doing better mixing?

10 MR. BURGER: Right. In the hottest --

11 DR. BANERJEE: And this is a fairly well
12 understood process?

13 MR. BURGER: Yes.

14 DR. BANERJEE: How much increase in DNB do
15 you get?

16 MR. BURGER: About a 20 percent increase.

17 DR. BANERJEE: Remarkable. And what about
18 the LOCA limits?

19 MR. BURGER: We'll go into that later in
20 the safety analysis and they'll actually show you the
21 markups of where the DNB margin limit, where the
22 correlation is, how much safety margin in. And we'll
23 go into that in the safety analysis.

24 DR. BANERJEE: So basically you have the
25 same surface area fuel, the same subdivision and

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1 you're getting 10 percent more power?

2 MEMBER SIEBER: Yes.

3 DR. BANERJEE: By doing something to the
4 DNB limit and the LOCA limits?

5 MEMBER SIEBER: Well --

6 DR. BANERJEE: Is that a correct
7 statement?

8 MEMBER SIEBER: Well, there's a couple of
9 effects going on. The other thing that gets effected
10 is the number of rods that have an increased peak clad
11 temperature during a LOCA, and usually with an
12 improved core design the approach to the 2200 degrees
13 doesn't change very much, but the number of rods who
14 make that approach does change because you're
15 flattening the power distribution.

16 MR. BURGER: Right. And you'll see that,
17 as we said, there's going to be 64 more feet
18 assemblies. So to get that extra power out, you'll
19 need more feed assemblies to go into the core. So
20 that's where you're getting extra power; you're going
21 to spread that power out over --

22 MEMBER SIEBER: That's where you get the
23 neutrons from.

24 DR. BANERJEE: You're not increasing the
25 surface area of the fuel? You're just bringing in

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1 fresher fuel?

2 MR. BURGER: Right. Distribute the burnup
3 along the assembly --

4 DR. BANERJEE: So that means you get a
5 high heat flux, too, right? So the issue really, and
6 hope you'll address is, is to understand how you can
7 get more power out of the same fuel, basically the
8 same fuel surface area. Maybe it's by sharpening the
9 pencils and doing a few experiments, but we want to be
10 convinced that this is really not. Maybe other people
11 have done that, but you would have to do it at some
12 point.

13 MR. FU: Okay. This Chun Fu, Westinghouse,
14 thermal hydraulic design.

15 So basically you have IFM, it enhance your
16 mixing an in an analysis area we have WRB-2M
17 correlation, which give you 20 percent or even a
18 little more than 20 percent in the margin. So you
19 will see that.

20 DR. BANERJEE: Yes, we'll look at it. And
21 the basis for it.

22 CHAIRMAN DENNING: This is probably an
23 irrelevant question, but why didn't you decide to go
24 to higher burnups?

25 MR. BURGER: Higher burnups?

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1 CHAIRMAN DENNING: Yes.

2 MR. BURGER: The average actually
3 discharge we're putting in four more assemblies.
4 You'll spread the burnup among those. So the average
5 discharge on the assemblies will remain about the
6 same. So you'll just put that burnup on more
7 assemblies. But you really, the overall will be in
8 the 50,000.

9 CHAIRMAN DENNING: What's your refueling
10 cycle then?

11 MR. BURGER: We're on 18 month refueling
12 cycles.

13 CHAIRMAN DENNING: You're on 18 month
14 refueling cycle?

15 MEMBER SIEBER: These are cycle burnups as
16 opposed to assembly burnups?

17 MR. BURGER: Discharge assembly will be in
18 the 50,000 --

19 MEMBER SIEBER: Right.

20 CHAIRMAN DENNING: That's what I didn't
21 understand.

22 MEMBER SIEBER: Which is a moderate. It's
23 sort of in the middle of where everybody's running.

24 MR. BURGER: Right. Yes. And there's
25 other plants that are operating at 5.69 and 2900 and

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1 they're in the similar area.

2 MEMBER SIEBER: Right.

3 MR. BURGER: Next slide.

4 Our current maximum riching is 5 weight
5 percent. We currently put in a split four of usually
6 495 right now and 46 enrichment, so it'll be no change
7 to the maximum enrichment that we'll see.

8 With T_{avg} remaining approximately the same
9 plus or minus 2 degrees of the current, you don't see
10 a whole lot of change in the flux profile on the
11 assemblies.

12 Again, we're operating with a full core of
13 RFA, full units so we won't have any transition four
14 penalties impacted.

15 And another item that we implemented was
16 separate from the EPU was RAOC. That was basically to
17 give more operating flexibility to the Operations.
18 They were doing that separately but when we went to
19 the EPU we also incorporated EPU conditions into the
20 RAOC curves that we came up with.

21 We've now implemented RAOC, start up of
22 Unit 1 here is with RAOC. So they're operating right
23 now with RAOC at the current --

24 MEMBER SIEBER: That's already been
25 approved?

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1 MR. BURGER: Yes, it's been approved.
2 Right. And we're actually operating it for the first
3 cycle right now.

4 MEMBER SIEBER: There are a number of
5 other plants that have already have this.

6 MR. BURGER: Right. And you have a tech
7 spec out of that one.

8 MEMBER SIEBER: Usually on the maximum
9 enrichment it's the spent fuel pool that governs how
10 high you can go.

11 MR. BURGER: Yes. We're currently at five
12 weight percent for both units.

13 MEMBER SIEBER: Okay. Do you take burnup
14 credit?

15 MR. BURGER: At Unit 1 we have Borel in
16 the Unit 1 fuel pool and so there's distinct regions
17 for that of where the fuel goes.

18 Unit 2 we have Borelfex. We're not
19 crediting the Borelfex in there. So we credit the
20 soluble boron in there. And we're trying to get a
21 rerack in there for Unit 2 to get rid of the Borel.
22 Also, to get more room in the spent fuel pool. And
23 that analysis will be done in the late 2009/2010 area.

24 MEMBER SIEBER: Do you have enough extra
25 spaces to wait that long?

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1 MR. BURGER: Apparently we can go that
2 long. We have submittal later this year for spent
3 fuel criticality analysis to maybe get a better
4 checkerboard pattern out of that and maximize those
5 areas in the pool.

6 MEMBER SIEBER: Well, the checkerboard
7 pattern ought to spread out the deposition of heat
8 modes, too.

9 MR. BURGER: Right. Exactly.

10 MEMBER SIEBER: For obvious reasons.
11 Okay.

12 MR. BURGER: And that's all I had in the
13 fuel and core design area.

14 CHAIRMAN DENNING: I think there is
15 something we want to pursue just a little bit here.
16 Because obviously we're on a tight time schedule
17 related to when we're going to have our full
18 Committee. And I see an issue here related to the
19 change in the DNB correlation associated with that
20 mixing. And I can see Sanjoy is ready to jump onto
21 this issue.

22 I'm wondering how quickly could we get
23 some information on the validation of this revision to
24 the DNB model? And presumably Westinghouse has some
25 results.

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1 MR. BURGER: Yes. That's already been
2 previously approved the correlation. And it's already
3 in use.

4 CHAIRMAN DENNING: Okay. So that's the
5 other element I wanted to --

6 MEMBER SIEBER: I think there's a WCAP on
7 that one.

8 MR. BURGER: Yes, there's a WCAP out there
9 for the WRB-2M right. And then we're applying it now
10 with the use of the VIPRE code and --

11 MEMBER SIEBER: Maybe we could just get a
12 copy of the WCAP?

13 MR. CARUSO: I can give you a copy of the
14 WCAP.

15 MEMBER SIEBER: Oh, okay.

16 DR. BANERJEE: And it's been applied to
17 this specific fuel?

18 MR. BURGER: Five or six years ago, yes.

19 DR. BANERJEE: To this specific fuel
20 design?

21 MR. BURGER: Yes.

22 DR. BANERJEE: And at these ratings?

23 MR. BURGER: Yes.

24 DR. BANERJEE: Where?

25 MEMBER SIEBER: Yes, before they sell it

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1 they usually have the correlation and have it
2 approved.

3 MR. CARUSO: The plants are using this
4 that have not done the uprate. Haven't done uprates.
5 They just use it to increase margin to improve their
6 fuel performance. There's a lot of reasons why they
7 would want to use that are --

8 DR. BANERJEE: So I think we could just
9 review what's being done right now.

10 MR. CARUSO: I think I can get a copy. I
11 know the guy who did the review.

12 DR. BANERJEE: Review the review?

13 MR. CARUSO: We could talk about that
14 offline. But that's not hard to get for you.

15 DR. BANERJEE: Okay.

16 CHAIRMAN DENNING: Okay. Very good. Thank
17 you very much.

18 We're now going to take a 15 minute break
19 and we start up again at five after 10:00.

20 (Whereupon, at 9:52 a.m. off the record
21 until 10:09 a.m.)

22 CHAIRMAN DENNING: Okay. We're now back
23 in session. And we're going to start up with Mr.
24 Frederick on safety analysis.

25 MR. FREDERICK: I wanted to thank the

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1 Committee for allowing us the opportunity to come and
2 talk to you.

3 As the slide says, my name is Ken
4 Frederick I'm the lead safety analyst at Beaver
5 Valley. By background I've worked at Beaver Valley
6 for 27 years, most of that time has been spent in the
7 engineering department, only a few years in the
8 operations.

9 For the last five years I've been assigned
10 to the uprate project and also the other projects that
11 we mentioned here, the containment conversion and the
12 best estimate LOCA.

13 Next slide.

14 Just to give you a brief objective for
15 what we consider the safety analysis of the plant.
16 First of all, we want to demonstrate that we have
17 compliance with all the regulatory limits and the
18 acceptance criteria . And also we want to show that
19 Beaver Valley has adequate safety margins at the EPU
20 conditions.

21 Next slide.

22 So basically we'll be talking about the
23 specific analysis areas that are listed here as well
24 as some of the methodologies and the setpoint changes
25 and design parameters associated with the EPU

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1 conditions.

2 This slide shows the design parameters for
3 the uprate condition as well as the current
4 operations. Basically here we're showing that the mass
5 flow through the reactor essentially is unchanged.
6 The thermal design flow, which is the tech spec value
7 which is in volumetric units gallons per minute stays
8 the same. So in order to get increased power out of
9 the core, we have to increase the enthalpy rise across
10 the core. So you see an increase in the hot leg
11 temperature and a slight decrease in the cold leg
12 temperatures.

13 CHAIRMAN DENNING: And the difference
14 between EPU low and EPU high is what?

15 MR. FREDERICK: We've analyzed a range for
16 T_{avg} . The low temperature being 566.2 and the upper
17 end is 580 degrees.

18 CHAIRMAN DENNING: And you would expect at
19 different times to be operating throughout that range
20 depending upon what was?

21 MR. FREDERICK: Yes, we have target
22 values. And you want to pull up the backup slide?

23 This slide shows the target values that
24 we're intending to operate at, although we could
25 revise the T_{avg} parameter in that range that we have

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1 the analyzed, 566.2 to 580.

2 For Unit 1 you can see T_{avg} as compared to
3 the current operation will go up a little less than 2
4 degrees. And the hot leg temperature will go up about
5 4 degrees.

6 And this is basically what we targeted and
7 we've optimized our turbine, our replacement high
8 pressure turbine for this steam pressure for the EPU
9 condition. Again, depending on our new generators,
10 our new replacement generators operate. And they do
11 seem to match up pretty well with the pre-EPU estimate
12 there of 822 psia. They're pretty much right on that.
13 So we probably won't be needing to make any
14 adjustments in T_{avg} but if --

15 MEMBER WALLIS: What do you mean psia?

16 MR. FREDERICK: Pardon me?

17 MEMBER WALLIS: Did you adjust for
18 atmospheric everyday? Don't you measure psig?

19 MR. FREDERICK: Yes. We actually measured
20 810 psig is what we're seeing out of the replacement
21 generators.

22 Move on to the next slide it shows the
23 Unit 2 target values. In Unit 2 we're actually
24 intending to reduce T_{avg} a couple of degrees. And the
25 intent here is to try and maintain the hot leg

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1 temperature at approximately where we are now, which
2 is at 609. That will minimize any impacts on the
3 materials.

4 MEMBER MAYNARD: Now Unit 2 is the one
5 that still has the 600 --

6 MR. FREDERICK: Yes.

7 MEMBER MAYNARD: Is that the main reason
8 you're trying to keep the --

9 MR. FREDERICK: That's correct.

10 MEMBER SIEBER: Unit 2 has 600? Okay.

11 MR. FREDERICK: And again, a T_{avg} results
12 in a reduced steam pressure here. So when we replace
13 our high pressure turbine in Unit 2, we'll be
14 targeting a lower steam pressure for the optimum
15 design in that turbine.

16 In the area of safety setpoints, we have
17 made a couple of changes to reactor trip setpoints.
18 Primarily these are the delta T trips, the
19 overpressure and over temperature delta T trips.

20 We've reduced the primary setpoint for
21 these trips. If you're familiar with the trips, that's
22 the K_1 and K_4 terms.

23 We've also added some filters on the
24 equations, the functional equations. I can pull up a
25 slide. You're looking puzzled, so we'll pull it up

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1 here.

2 MEMBER WALLIS: I'm puzzled.

3 MR. FREDERICK: This is the actual
4 equation that models this trip. And again, that's all
5 done electronically.

6 The K_1 term for the OT delta T trip and
7 the K_4 term for the OPR, the primary trip and then the
8 rest of the terms there are basically lag and lead
9 functions and also some adjustments based on actual
10 temperature and pressure conditions.

11 MEMBER WALLIS: How long are these times
12 typically that are in the --

13 MR. MURTAGH: This is Brian Murtagh.

14 The filtering is about 6 seconds for the
15 T_{avg} and delta T filters. All the other time
16 constraints are typically for the lead lag function
17 would be 30 over 4. Tile 1 and tile 2 would be tile
18 130, tile 24.

19 MR. FREDERICK: Does that answer your
20 question?

21 MEMBER WALLIS: Yes. I was just going to
22 get an order of magnitude of the tiles to see what
23 sort of times you're dealing with.

24 MR. FREDERICK: Right. The filters,
25 again, were added essentially to give us additional

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1 operating margin so we don't see inadvertent trips
2 from temperature spikes and that type of thing.

3 MEMBER WALLIS: To wipe out the bouncing
4 array?

5 MR. FREDERICK: The noise, right.
6 Correct. And with the reduced trip setpoint and the
7 additional filters we're not really losing any
8 operating margins.

9 Some other --

10 DR. BANERJEE: Does this sort of take out
11 some specific frequency component and above? When
12 looking at this equation I can't tell anything. So
13 what is the frequency cut off --

14 MR. FREDERICK: Brian?

15 MR. MURTAGH: Well, if you were to look at
16 it in terms of a low pass filter --

17 DR. BANERJEE: Yes.

18 MR. MURTAGH: -- then the cut of frequency
19 would be the inverse of one over 6 seconds, say.

20 DR. BANERJEE: One over 6 seconds?

21 MR. MURTAGH: Yes.

22 DR. BANERJEE: Why 6 seconds? Why not 10,
23 why not 3?

24 MR. MURTAGH: Well, I believe probably as
25 much as you increase the filtering, you're going to

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1 have to decrease the setpoints. Okay. So it's an
2 optimization of how you want the circuit to function.
3 You know, it's a trade off between that protects part
4 of it --

5 MEMBER WALLIS: If it's too long, then you
6 don't respond quickly enough.

7 MR. MURTAGH: Right.

8 MEMBER WALLIS: And if it's too short, you
9 respond to every little transient.

10 MR. MURTAGH: And if it doesn't respond
11 quickly enough, you'll have to reduce the set point.

12 DR. BANERJEE: So is this judgment call?
13 Is it a judgment call or is it an optimization?
14 Optimization assumes there's a function you're trying
15 to maximize, right?

16 MR. MURTAGH: Yes. I believe the code for
17 it is OptiMax code -- OptoX code used by Westinghouse.

18 DR. BANERJEE: What is it you're trying to
19 optimize?

20 MR. DURKOSH: This is Don Durkosh.

21 What I wanted to point out was the time
22 constants here. These were established many years ago
23 at Westinghouse and they were optimized based on the
24 plant design. And for the most part these constants
25 have stayed pretty much the same and have been used by

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1 just about all Westinghouse plants.

2 As part of this project all they did was
3 they looked at this and they tried to optimize. As
4 Ken pointed out, what they did was they lowered the
5 steady state trip value of small mount and by doing
6 that they were able to add a small time delay so that
7 if a particular noise event occurred, it wouldn't
8 bring that channel into a partial trip condition. So
9 it's just a small trade off as steady state versus a
10 transient change.

11 DR. BANERJEE: So how small was this?
12 What was small here?

13 MR. DURKOSH: Well, I don't have the
14 numbers memorized, but I did talk to the Westinghouse
15 and-- DR. BANERJEE: Rough terms.

16 MR. DURKOSH: Basically these values are
17 representative of what other plants have. They are
18 not out of line.

19 MEMBER KRESS: Don't you need some sort of
20 measure of the normal oscillations to do this
21 optimization?

22 DR. BANERJEE: What does that mean in
23 delta T? I can't tell that with the ratio?

24 MR. DURKOSH: Well, let's take the first
25 bullet here.

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1 DR. BANERJEE: Yes.

2 MR. DURKOSH: At steady state conditions
3 for K_1 , 1.259. What that means is if loop delta T got
4 up to 25.9 percent above nominal, it would actuate.
5 So we've lowered that value a little bit. We've
6 reduced the steady state trip value from 25.9 percent
7 to 24.2 percent at Unit 1. And we traded that margin
8 off against just delaying the signal and the length of
9 the signal that requires actuation.

10 DR. BANERJEE: By how much? It would be
11 nice to have real numbers instead of percentages
12 because I can't tell what they are looking at them.
13 Whether there's a degree, 10 degrees, 5 degrees; what
14 is the number?

15 MEMBER WALLIS: Well, I guess our interest
16 would be --

17 MR. DURKOSH: The number for --

18 DR. BANERJEE: How many seconds, how much
19 average --

20 MR. MURTAGH: The K_1 number means for your
21 at nominal delta T that you have measured at 100
22 percent power. If you reach a 124 percent of that
23 value, you will trip.

24 DR. BANERJEE: Right. But you know the
25 normal operating temperature --

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1 MR. FREDERICK: The nominal delta T is
2 about 60 degrees.

3 DR. BANERJEE: Sixty degrees?

4 MR. FREDERICK: Right.

5 DR. BANERJEE: So you've reduced that by
6 how many degrees?

7 MR. FREDERICK: The trip?

8 MR. MURTAGH: The trip will be 124 percent
9 of the nominal value.

10 MR. FREDERICK: Well, 2 percent of 60 is
11 roughly one degree.

12 DR. BANERJEE: This is my head, I need a
13 calculator.

14 MR. FREDERICK: It's roughly 1 degree
15 delta.

16 DR. BANERJEE: Okay. One degree. And the
17 time?

18 MR. FREDERICK: I'm not sure. Brian, do
19 you know what the time change was? In addition to the
20 filter, what does it --

21 MR. MURTAGH: Well, there's no direct
22 correlation between filtering and --

23 MEMBER WALLIS: The only thing that
24 matters to me really is the impact of these things on
25 the plant.

1 DR. BANERJEE: Yes. So one degree change
2 is a small change, but that has given you a big change
3 in the time available?

4 MR. MURTAGH: Has that given you a big
5 change?

6 DR. BANERJEE: How much?

7 MR. MURTAGH: The time delay is going to
8 be built into the safety analysis where the function
9 is no longer credited as an immediate trip. It would
10 be assumed to be delayed in a safety analysis.

11 DR. BANERJEE: By how much?

12 MR. FREDERICK: If I understand what
13 you're asking, we'll get that number for you.

14 DR. BANERJEE: You know, I just want to
15 get a feel for does 1 degree change in this give you
16 twice as much time or is it --

17 MR. FREDERICK: Yes, I understand.

18 DR. BANERJEE: -- five percent, or
19 nothing?

20 MR. FREDERICK: We'll have to get back to
21 you on that.

22 MEMBER SIEBER: Well, there's an inherent
23 time delay anyway.

24 DR. BANERJEE: If it's small, it's
25 irrelevant. Yes.

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1 MEMBER SIEBER: That's because of the
2 instrument response.

3 DR. BANERJEE: Yes.

4 MEMBER MAYNARD: But it's still a trade
5 off, but you're not approaching any limits anymore.
6 You're trading off the point at which it trips or a
7 time. It's still within that time. It can't exceed
8 any of your safety analysis requirements or anything.
9 So it's not changing a limit that you're going to get
10 to.

11 MEMBER SIEBER: Right.

12 DR. BANERJEE: Anyway, appreciate having
13 the time.

14 MEMBER WALLIS: And I think our main
15 message should be it changes to what? What's the
16 adverse consequence because we haven't said anything
17 about the consequence here.

18 MR. FREDERICK: Right. Yes, the delta T
19 trips are primarily DNBR protection trips --

20 MEMBER WALLIS: So the thing is by
21 changing this, have you reduced the DNBR margin
22 significantly? That's what really we should look at?

23 MR. FREDERICK: Yes.

24 MEMBER WALLIS: Maybe you could tell us--

25 MR. FREDERICK: Yes, well we'll talk about

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1 that in some detail later.

2 MEMBER WALLIS: We'll get to that, I
3 presume.

4 MR. FREDERICK: Right. Right.

5 MEMBER WALLIS: You heard about how we
6 probed the last applicant on this question?

7 MR. FREDERICK: Yes. Yes.

8 MEMBER WALLIS: Thank you.

9 MR. FREDERICK: Okay. Let me go back to
10 the original slide here.

11 Other protection system changes. We've
12 changed the low steam generator level trip for Unit 1,
13 and that's associated with changes in the instrument
14 span for that replacement generator. Has a larger,
15 narrow range span.

16 Again, as we talked about before, we were
17 eliminating the flux rate trip. And that, again, was
18 a generic approved, not associated with EPU, but
19 included.

20 The containment set point changes were
21 associated with containment conversion. Those have
22 already been implemented. We've raised the setpoint
23 since we've increased the normal operating pressure.

24 And we also at that time, we revised the
25 low level RWST recirc setpoint. And that was --

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1 MEMBER WALLIS: You went from a reduced
2 pressure containment to an atmospheric, is that what
3 happened?

4 MR. FREDERICK: That's correct.

5 MEMBER WALLIS: Why did you do that?
6 Maybe you've explained that already, but why?

7 MR. FREDERICK: Yes, we can talk about it
8 later. But primarily the reason is --

9 MEMBER SIEBER: To make old guys breath
10 easier, right?

11 MR. FREDERICK: That is a very key factor,
12 yes. We have an aging workforce and wearing 40 pound
13 biopacks in containment is certainly not very
14 comfortable. So it does add a --

15 MEMBER WALLIS: An aging workforce is
16 what--maybe we should pressurize this room.

17 DR. BANERJEE: Oxygenate.

18 MR. FREDERICK: Consideration of personnel
19 safety and we also see some other benefits in the
20 analysis from the increased pressure. And we'll talk
21 about that later.

22 DR. BANERJEE: What is the RWST level low-
23 low setpoint lowered? What is the implication of
24 this?

25 MEMBER SIEBER: I'm sure safety injection

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1 is --

2 MR. FREDERICK: The setpoint is where
3 transfer from injection mode to recirc mode. And by
4 lowering that setpoint we end up with more water in
5 the sump whenever we do that transfer so that
6 increased the NPSH margin for primarily the low head
7 safety injection pumps.

8 DR. BANERJEE: Do you have a problem with
9 NPSH margin?

10 MR. FREDERICK: Yes, we're pretty close to
11 the limit.

12 DR. BANERJEE: Is that why you're doing
13 that?

14 MR. FREDERICK: That was one of the
15 reasons, yes.

16 DR. BANERJEE: And the water is hotter
17 because your containment is at a higher pressure now?

18 MR. FREDERICK: Yes. It is slightly
19 higher. And we'll talk about some of that in the
20 containment portion of the --

21 MEMBER SIEBER: Yes, that shouldn't be by
22 much, though.

23 MR. FREDERICK: Yes.

24 Next slide, please.

25 We have changed some of the control system

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1 setpoints. Again, these were just setpoint changes,
2 none of the control schemes were function changes in
3 the plant.

4 Pressurizer level is something that's
5 programmed to T_{avg} so that the maximum or the normal
6 operating level is a function of what T_{avg} we're
7 operating at. So raising T_{avg} a couple of degrees will
8 increase pressurizer level by a couple of percent of
9 full power.

10 MEMBER SIEBER: Well the controller will
11 do that, but you program it to make it happen, right?

12 MR. FREDERICK: Yes. There is a little
13 rescaling involved. But, yes.

14 MEMBER SIEBER: I take it you've analyzed
15 the response of the pressurizer for various transients
16 and accidents to show that it is still of adequate
17 size?

18 MR. FREDERICK: Yes. We've analyzed for
19 the full range of accidents and also margin to trip
20 analyses.

21 MEMBER SIEBER: Okay.

22 MR. FREDERICK: The more normal
23 occurrences. And we'll talk about it --

24 MEMBER SIEBER: And the change you're
25 making is not that great, so it shouldn't have a big

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1 impact on the pressurizer size.

2 MR. FREDERICK: Right. Right.

3 MEMBER SIEBER: Okay.

4 MR. FREDERICK: We're also changing some
5 of the steam dump. This is essentially the turbine
6 bypass system. The control setpoints there are
7 optimized to operate for the EPU condition.

8 Steam generator level again for Unit 1
9 with the replacement generator, we have to increase
10 the setpoint for normal water level. Essentially it
11 stayed the same where we were before because of the
12 increased span on the tape settings.

13 DR. BANERJEE: I didn't get that last
14 point. Why did you have to increase the --

15 MR. FREDERICK: The replacement steam
16 generators, they have a 212 inch span for the narrow
17 range. The old ones had about 144 inch range. So to
18 get to the same level now we're at 65 percent, which
19 before we were at 44 percent. So it's just a change
20 based on the span.

21 Next slide.

22 MEMBER SIEBER: These slides that have the
23 little boxes like this one to the right, that's a
24 backup slide?

25 MR. FREDERICK: That's correct.

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1 MEMBER SIEBER: Are they in this book some
2 place?

3 MR. FREDERICK: No, they're not. We do
4 have copies available.

5 MEMBER SIEBER: I think we would need the
6 copies of the slides that you show?

7 MR. CARUSO: I have those. I'll print them
8 up for you. I have an electronic copy of this.

9 MEMBER SIEBER: Oh, okay.

10 DR. BANERJEE: If you have an electronic
11 copy of all this --

12 MEMBER SIEBER: Why don't you just give us
13 the electronic copy and --

14 DR. BANERJEE: So then we just may get the
15 electronic copy from you rather than this.

16 MR. CARUSO: Sure.

17 MR. FREDERICK: This slide basically
18 outlines the methodologies that we used for the safety
19 analysis. And it also shows what the current
20 methodologies were. So for large break LOCA we are
21 changing from the Westinghouse BASH methodology, which
22 was Appendix K method, to the BE LOCA methodology,
23 which uses the COBRA/TRAC code.

24 And as we mentioned previously, this is
25 the original BE LOCA methodology approved in 1996 when

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1 we started this program, ASTRUM, which is what Ginna
2 used, wasn't approved at that time. So we're not using
3 that.

4 DR. BANERJEE: Do you do these
5 calculations yourself or somebody else does it?

6 MR. FREDERICK: Westinghouse has performed
7 these calculations for us.

8 DR. BANERJEE: I see.

9 MEMBER SIEBER: You have access to their
10 codes, though, right?

11 MR. FREDERICK: I have access to LOFTRAN,
12 but not the LOCA codes. Just the non-LOCA.

13 DR. BANERJEE: So you sort of contract
14 them to do this work?

15 MR. FREDERICK: That's correct.

16 DR. BANERJEE: And how much audit
17 capability do you have of what's going on there?

18 MR. FREDERICK: We have reviewed all of
19 the calculations that were done for the uprate. In
20 other words --

21 DR. BANERJEE: You don't have a copy of
22 the code to test out or anything like that?

23 MR. FREDERICK: Well, again, in the case
24 of non-LOCA I do have a copy of the LOFTRAN code which
25 I do run. I don't have a copy of NOTRUMP or

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1 COBRA/TRAC. Our review is basically limited to making
2 sure that they use the inputs that we specify and
3 making sure the output looks reasonable.

4 As I mentioned, large break we have
5 changed to BE LOCA. The small break still uses
6 NOTRUMP, which is the Westinghouse small break
7 approved methodology.

8 MEMBER WALLIS: Now you've changed to best
9 estimate method. Did you try to use BASH on the power
10 uprate?

11 MR. FREDERICK: No, we did not.

12 MEMBER WALLIS: Because I was wondering if
13 you would be over the limit if you used it? Did you
14 use BE LOCA because you have to because otherwise
15 you'd--

16 MR. FREDERICK: It was a decision that we
17 made to regain some margin which would help us out
18 with the --

19 MEMBER WALLIS: It's so conservative. It
20 looks like it would drive you over the limit if you
21 gain power too much.

22 MR. TESTA: Ken, if I can input here. I'm
23 Mike Testa, I'm the Project Manager at Beaver Valley.

24 When we first set out on this project with
25 the extended power uprate, you know, we were going to

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1 do an extensive reanalysis. And part of that is we
2 wanted to bring the design up to the later design
3 codes. So that was an opportunity for us. We knew we
4 had to redo the LOCA analysis and we choose to go to
5 the BE LOCA methodology.

6 MEMBER WALLIS: And my question really was
7 if you'd used BASH, because I'd like to compare the
8 new with the old when you give us, say, 2190 degrees
9 or something.

10 MR. TESTA: Yes. We did not run--

11 MEMBER WALLIS: And maybe the temperature
12 actually goes down with the new prediction method
13 because it's because of the method, rather than the
14 physics.

15 MR. FREDERICK: Yes. But we did not run
16 that.

17 MEMBER WALLIS: But I think we'll get into
18 that later, perhaps.

19 DR. BANERJEE: Was there industry
20 experience with something equivalent to BASH that
21 suggested you should do BE LOCA?

22 MR. FREDERICK: Certainly the BE LOCA was
23 known to provide better results just because of the
24 methodology --

25 DR. BANERJEE: There were lower --

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1 MEMBER SIEBER: That's correct. Yes.

2 DR. BANERJEE: Lower results? Better we
3 don't know for sure.

4 MEMBER WALLIS: From the point of view of
5 safety, better is higher.

6 DR. BANERJEE: Better results?

7 MEMBER SIEBER: Lower results.

8 MEMBER WALLIS: Because then you could
9 back off.

10 MEMBER SIEBER: Well, there is a typical
11 for BE LOCA in an SER which would -- I don't know
12 whether that --

13 MR. FREDERICK: This version of BE LOCA
14 was actually approved in 1996 and a lot of other
15 plants have been using it.

16 DR. BANERJEE: Yes, but --

17 MEMBER SIEBER: You may want to look at
18 that topical in the SER to determine what the
19 equivalence, if any, there is. Because there probably
20 isn't much of an equivalence because one uses an
21 extreme boundaries of everything whereas BE LOCA is
22 best estimate with uncertainty. Get a different
23 answer.

24 MR. CARUSO: I believe the Committee has
25 written a letter on this method.

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1 MEMBER SIEBER: I suspect they have.

2 MEMBER WALLIS: Well, it came up with the
3 last applicant that they had used the Appendix K
4 method. I think they went over 2200 degrees. BE LOCA
5 put them way below. So it makes a big difference.

6 MEMBER SIEBER: Yes.

7 DR. BANERJEE: But going back, I just want
8 to be -- have any of these other uprates that were
9 listed which are somewhat similar to these used
10 something equivalent to BASH in doing that, do you
11 know?

12 MR. FREDERICK: I don't know. I'm sure
13 that some of the older uprates would have used BASH
14 because that was what the licensed code was at that
15 time.

16 Matt, do you have any --

17 MR. CERRONE: Yes. Hi. My name is Matt
18 Cerrone with Westinghouse.

19 All recent uprates are all done with best
20 estimate methods for the large break accident.

21 DR. BANERJEE: When was the last one done
22 with BASH?

23 MR. CERRONE: I don't know.

24 DR. BANERJEE: Was there one done with
25 BASH?

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1 MR. CERRONE: I can't imagine. I mean, my
2 experience would have it that -- basically all my
3 experience with Westinghouse was whenever we would
4 move to a new product or especially with uprates, the
5 best estimate technology using COBRA/TRAC is the
6 methodology of choice because it is capable of
7 modeling the phenomena that's expected out of these
8 codes for large break accidents these days.

9 DR. BANERJEE: Now just to follow this.
10 The BASH number for the unuprated plant were
11 acceptable, I take it? Now, this 10 percent increase
12 must then give some problem with BASH, otherwise why
13 would people go running to the best estimate.

14 MR. FREDERICK: I do have a slide later
15 that shows the BASH results with current power level.

16 MEMBER WALLIS: I take it we're going to
17 get into each of these in detail later on?

18 MR. FREDERICK: That's correct.

19 MEMBER WALLIS: Okay.

20 MEMBER KRESS: When you do the large break
21 LOCA did you take advantage of the new break size that
22 NRC is flirting with?

23 MR. FREDERICK: No, we did not.

24 MEMBER KRESS: You used the actual large
25 double winded --

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1 MR. FREDERICK: Yes, double winded
2 rupture.

3 MEMBER SIEBER: When you did the
4 calculations for the alternate source term in your
5 containment parameters, you used the latest DKE curve?
6 Does BELOCA use the same DKE curve or the earlier
7 versions that the Appendix K used?

8 MR. FREDERICK: BE LOCA methodology uses
9 the 79 curve with 2 sigma, not the 71.

10 MEMBER SIEBER: Okay. That's the later?

11 MR. FREDERICK: That's correct.

12 For non-LOCA events we've changed the DNBR
13 calculation methodology from THINC to VIPRE. LOFTRAN
14 is still used for the thermal hydraulics.

15 In the containment area again, as part of
16 the containment conversion submittal which was
17 recently approved, we have gone to MAAP-DBA.
18 Previously we used a Stone & Webster code named
19 LOCTIC, called LOCTIC.

20 And again, in dose assessment area we have
21 implemented -- we have gone to a full implementation
22 of the alternative source term and we're also using
23 ARCON 96 now for on-site --calculations.

24 Essentially this is just a list of the
25 non-LOCA events that we've analyzed or evaluated.

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1 These are categorized by the Standard Review Plan
2 categories. I'm not going to read them all. You can
3 look at them there. The next couple of slides here.
4 In total there's 18 events in the non-LOCA area that
5 were again looked at for EPU and these have new
6 analyses associated with them.

7 MEMBER WALLIS: You're going to give us a
8 table of results somewhere?

9 MR. FREDERICK: Yes, we'll get into that.
10 For condition II events which comprises a
11 majority of the non-LOCA events, the acceptance
12 criteria are meet the DNBR limits, heat generate rate
13 has to remain within the acceptable limits. The RCS
14 and the secondary pressures need to stable to 110
15 percent of the design. And the event cannot progress
16 to a more series level 3 or level 4 event.

17 DR. BANERJEE: Does this also apply for
18 steam line breaks?

19 MR. FREDERICK: Yes. Well, steam line
20 break, as we'll see, is actually a condition IV event.
21 But when we analyze it we use condition II criteria.
22 So it does apply, yes.

23 MEMBER WALLIS: Now you've seen these
24 slides before. Is something wrong with the screen
25 here? Is that why it doesn't look good?

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1 DR. BANERJEE: Yes.

2 MEMBER WALLIS: Why did the NRC, we
3 designed this room and give us a far worse screen than
4 we had before.

5 MEMBER KRESS: That's a good question.

6 MEMBER WALLIS: I think we should put that
7 on the record.

8 CHAIRMAN DENNING: I don't think we're
9 going to demand that you answer that.

10 MEMBER WALLIS: Well, I just want to make
11 sure it's not just me. I mean, when you get --

12 MEMBER KRESS: It's not just you. Rest
13 your eyes.

14 MEMBER WALLIS: It's a good slide.

15 MR. FREDERICK: Next slide.

16 The first acceptance criteria we're going
17 to talk about is the DNBR limits. As we mentioned
18 earlier, DNBR is calculated using approved
19 correlations. For Beaver Valley we use three
20 correlations, WRB-1. WRB-2M and W-3. And the
21 application of these is essentially controlled by what
22 conditions they're approved for and also what the
23 operating conditions are for the analysis. And we'll
24 get into some examples later.

25 Primarily WRB-2M is used because that is

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1 specifically for the RFA fuel, which we use, and for
2 the high temperature regions of the fuel with the
3 mixing vanes.

4 Something else that's used here is called
5 revised design thermal design procedure. And that is
6 a methodology, again an NRC approved method which
7 takes the uncertainties on power, flow, temperature
8 and pressure and combines those into essentially a
9 penalty that's applied to the DNBR limits. And we'll
10 see that again on the next slide.

11 One thing to mention here is that at
12 Beaver Valley, primarily because of the change to WRB-
13 2M and the RFA fuel we actually have 21 percent margin
14 between what we use as a safety analysis limit and the
15 actual design limits for the fuel. And essentially
16 that margin is retained to give the core designer some
17 flexibility in the reload process so that if an issue
18 comes up or a penalty that needs to be applied and
19 they have the flexibility to do that without having to
20 go back and redo all the safety analysis.

21 So if you look at the next slide, this
22 kind of gives you a picture of how the limits are
23 developed. On the left is the DNBR ratio. And on the
24 right is the corresponding limit. So 1.0 obviously is
25 critical heat flux.

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1 The correlation limit is actually a tech
2 spec value and it reflects the uncertainty in the
3 correlation that corresponds to the 95/95 confidence
4 level.

5 From there we go up to 1.22, which is what
6 we get when we add in the uncertainties associated
7 with the initial conditions in the core for power
8 flow, pressure and temperature.

9 And finally, the 1.55 is what we're using
10 as the safety analysis limit. So in between the 1.22
11 and the 1.55 essentially is margin which is retained
12 by the thermal hydraulic people in the --

13 MEMBER WALLIS: Now the previous applicant
14 used 1.38.

15 MR. FREDERICK: That's correct.

16 MEMBER WALLIS: So it seems there's a lot
17 of flexibility in what you choose to use.

18 MR. FREDERICK: Yes. That limit is
19 something that is somewhat negotiated between the fuel
20 designers and the safety analysis people within
21 Westinghouse in this case.

22 MEMBER WALLIS: So should we give you high
23 marks for having a high DNBR? More safety,
24 presumably.

25 MR. FREDERICK: Yes. The limit is set

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1 high primarily because in the past we had transition
2 core penalties which have since gone away since we're
3 into all RFA fuel at this point. But we haven't
4 changed the limit.

5 MEMBER WALLIS: I wasn't here earlier. Are
6 you changing the fuel when you do the uprate?

7 MR. FREDERICK: No.

8 MEMBER WALLIS: Not at all?

9 DR. BANERJEE: But it's all RFA fuel?

10 MEMBER SIEBER: I guess the more important
11 question when you talk about margins is do you have
12 somebody in your organization who is the keeper of
13 margins? For example, you know there are things you
14 can do when you refuel the reactor if you don't put in
15 the flow limiting devices, that changes the core flow
16 significantly and trades margin around. And if you
17 don't have a single person who is watching what the
18 condition of the core and all the modifications to the
19 plant and changes in operating procedures, you may be
20 giving up margin that you would rather have someplace
21 else, or maybe two people taking a bite out of the
22 same margin unbeknownst to one another.

23 MR. FREDERICK: Right.

24 MEMBER SIEBER: Do you have somebody that
25 does that?

1 MR. FREDERICK: Well, primarily that's me,
2 yes. We're very aware --

3 MEMBER SIEBER: Do you do a good job of
4 that?

5 MR. FREDERICK: I think so.

6 MEMBER SIEBER: You want to write that
7 down?

8 MR. FREDERICK: I'm very aware of where
9 our margins lie, particularly in terms of accident
10 analysis, results, PCTs for LOCA events and DNBR
11 margins. Those values are associated are actually
12 published every time we do a reload safety analysis.
13 So we understand what the margins are and we provide
14 the majority of the inputs for the reload evaluation.
15 So there's margins that have to move around or to
16 trade off operating margins. And we're part of that
17 process and we're aware of it.

18 MEMBER SIEBER: And so are you on the on-
19 site safety committee?

20 MR. FREDERICK: No, I'm not.

21 MEMBER SIEBER: But you are the keeper of
22 the margin.

23 MR. FREDERICK: Our on-site safety
24 committee--

25 MEMBER SIEBER: Do you have somebody in

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1 your organization who is on that committee?

2 MR. FREDERICK: We do.

3 MEMBER SIEBER: Okay. Since you're the
4 keeper of the margin --

5 MR. FREDERICK: He sits right across from
6 me, so --

7 MEMBER SIEBER: Okay.

8 MR. MANOLERAS: Yes, Jack. And this Mark
9 Manoleras.

10 We do sit on the Core Reload Safety
11 Process. We have a sign-off on that, a design
12 engineering manager and Ken. We have a sign-off on
13 that Core Reload Safety Process. We have a direct
14 input to that process.

15 MEMBER SIEBER: Okay. Yes, what I concern
16 myself with is sometimes there are subtle little
17 changes in the operation and maintenance of the plant
18 that can change these margins.

19 MR. BURGER: Yes. This A.R. Burger again.

20 What we do in the core design process, we
21 have a reload project team. Ken will be part of that.
22 We have operations training, chemistry, design
23 engineering. What we'll do is look at that on each
24 reload and decide: (a) what changes are being made in
25 the plant with other items that are out there and then

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1 we'll determine where we can put our DNB margin based
2 on what's going on in each reload.

3 MEMBER SIEBER: And the refueling
4 supervisor is part of that?

5 MR. BURGER: Yes.

6 MEMBER SIEBER: Okay.

7 MR. FREDERICK: Can I move on? Okay.

8 This is a table that shows the results for
9 events which primarily are looked at for DNBR as one
10 of their limits. And as you can see here, some of the
11 events use correlations other than WRB-2M. For
12 example, the first one is a rod withdrawal from
13 subcritical so the correlation essentially does not
14 apply in that power range, so we used W-3 and WRB-1
15 which are applicable at that condition.

16 Also for the hot zero power steamline
17 rupture we used W-3 for that. For similar reasons it's
18 not a full power event.

19 CHAIRMAN DENNING: And the reason on the
20 first one, the RCCA bank withdrawal was acceptable is
21 you believe the 1.65 on the W-3 more than the WRB-1 or
22 what's --

23 MR. FREDERICK: Actually, Chun, maybe you
24 can explain this. But both of those are used in
25 various regions of the --

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1 MR. FU: This is Chun Fu, Westinghouse.

2 The used of WRB-1 correlation is because
3 for this rod withdrawal from subcritical the similar
4 condition is out of the applicable range of WRB-2M
5 correlation. But we did confirm, you know, that DNB
6 criteria is met with WRB-1 correlation.

7 MR. FREDERICK: I think he was asking why
8 we used both W-3 and WRB-1.

9 MR. FU: Both W-3 correlation, you know,
10 WRB-1, WRB-2M correlation is applicable only for the
11 mixing in grid spans. So we still use W-3 for the
12 first span just from the inlet to the first mixing
13 grid. So W-3 is always correlation.

14 MR. FREDERICK: So it's the position on
15 the fuel rod where --

16 MEMBER WALLIS: So this doesn't indicate
17 two different results from two correlations for the
18 same place?

19 MR. FREDERICK: That's correct.

20 MEMBER WALLIS: It's different places,
21 right?

22 MR. FREDERICK: Yes.

23 As you can see here the limiting case in
24 terms of DNBR margin is the rod withdrawal of power
25 event. And we're going to talk about that in some more

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1 detail here in a little bit.

2 CHAIRMAN DENNING: How does the positive
3 moderator coefficient impact some of these as far as
4 if you had zero moderator coefficient versus the small
5 positive? Is it measurable in terms of the DNBR as to
6 what result you get?

7 MR. FREDERICK: Chun, could you answer
8 that?

9 MR. FU: I don't know --

10 MR. McHUGH: This is Chris McHugh from
11 Westinghouse.

12 The positive moderator temperature
13 coefficient does show up in the analysis if you have
14 a heat up event and you analyze the zero MTC versus a
15 small positive, you will see a difference in the
16 results.

17 To correlate that to a change in DNBR
18 would be a function of which event you're talking
19 about.

20 CHAIRMAN DENNING: But for example in this
21 bank withdrawal of power, is that --

22 MR. McHUGH: In the bank withdrawal at
23 power --

24 MEMBER SIEBER: It would be part of it.

25 MR. McHUGH: It would be a small penalty,

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1 yes.

2 MR. FREDERICK: As I mentioned earlier,
3 the steamline ruptures are actually condition IV
4 events but we do analyze them to the DNBR --

5 MEMBER WALLIS: Now there seem to be fewer
6 items in this table than there were on pages 33536?

7 MR. FREDERICK: Yes. Again, these are
8 primarily the events which challenge the DNBR limits.

9 MEMBER WALLIS: We have to assume that the
10 other ones are milder?

11 MR. FREDERICK: Either they're not
12 analyzed for DNBR because of the nature of the event
13 would not cause DNBR to decrease or they're just not
14 anywhere near limiting.

15 MEMBER WALLIS: But how do you evaluate
16 something like uncontrolled boron dilution? Are you
17 going to tell us that or --

18 MR. FREDERICK: Chris, can you answer
19 that?

20 MR. McHUGH: We do an uncontrolled boron
21 dilution calculation. We take the active mixing
22 volume, the initial and critical boron concentrations
23 and calculate a time that it takes to dilute it and
24 lose shutdown --

25 MEMBER WALLIS: You say that the operators

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1 have enough time to take action?

2 MR. McHUGH: Right. We conclude that they
3 have in excess of 15 minutes.

4 MEMBER WALLIS: You don't calculate any
5 kind of adverse effect. You just assume it's avoided?

6 MR. McHUGH: Right.

7 MR. FREDERICK: Next slide.

8 CHAIRMAN DENNING: One more thing, and
9 that is pre EPU what did the RCCA bank withdrawal look
10 like.

11 MR. FREDERICK: I have that on that slide
12 when we talk about that event.

13 CHAIRMAN DENNING: Okay.

14 MR. FREDERICK: One of the other key
15 criteria for the condition II events in the RCS or
16 primary and secondary pressure. This shows the primary
17 pressure limits in terms of how they correspond to the
18 ASME service level stress limits. So, for example,
19 starting at the bottom there at 2250 is our normal
20 operating pressure. The design pressure system is
21 2485 psig. For service level B, which is used for
22 condition II events, the ASME stress limit is 1.1
23 times the allowable stress. Conservably, that's just
24 taken to mean a 110 percent of the design pressure
25 even though if you looked at every component, you may

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1 be able to exceed 110 percent of design.

2 Similarly for level C we use a
3 conservative criteria for locked rotor of 120 percent.
4 Locked rotor is a condition IV event.

5 For ATWS the approach taken there was to
6 actually go and look at all the components. And the
7 limit arrived at in that manner was 3200 psig. So
8 that is the limits applied to ATWS events.

9 MEMBER WALLIS: Again, these pressures
10 aren't all to be engaged because that's what the
11 vessel fields, isn't it?

12 MR. FREDERICK: That's correct.

13 MEMBER WALLIS: The vessel doesn't know
14 anything about absolute pressure.

15 MR. FREDERICK: The analyses --

16 MEMBER WALLIS: If you put it in a
17 different containment --

18 MEMBER SIEBER: Do you happen to know the
19 number where you would actually get a failure of the
20 vessel?

21 DR. BANERJEE: You could have a vacuum.

22 MEMBER WALLIS: Never been tested, has it?

23 MR. FREDERICK: Yes. I don't know that
24 number, Jack. 3200 was based on --

25 MEMBER SIEBER: It's like three times 25,

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1 right?

2 MR. FREDERICK: Yes.

3 MEMBER SIEBER: Twenty-five hundred?

4 MEMBER WALLIS: Seven thousand psi or
5 something like that?

6 MEMBER SIEBER: Yes, something like that.

7 MEMBER WALLIS: Because it stretches bolts
8 before that.

9 MEMBER SIEBER: Well, I would be heading
10 out of town if it was going up there.

11 MR. FREDERICK: This table shows the
12 results from the events which challenge the over
13 pressure limits. As you can see here, loss of load is
14 a limiting event for condition II events. At 2747 for
15 Unit 1 --

16 MEMBER WALLIS: That's pretty close, isn't
17 it? That's pretty close.

18 MR. FREDERICK: Yes. We're going to talk
19 about that event in more detail soon.

20 MEMBER WALLIS: No uncertainty? This is
21 just one spot calculation, best estimate?

22 MR. FREDERICK: No. This is a very
23 conservative analysis, and that's what we're going to
24 demonstrate.

25 MEMBER WALLIS: That's why it's okay.

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1 MR. FREDERICK: This also shows locked
2 rotor, which again is below the 120 percent limit and
3 the ATWS analyses for both units.

4 DR. BANERJEE: What were these limits
5 before the uprate?

6 MR. FREDERICK: The limits have not
7 changed.

8 MEMBER WALLIS: No, but what were your
9 values?

10 DR. BANERJEE: I mean the peak primary
11 pressure values?

12 MR. FREDERICK: I do have that for the
13 limiting case here. The loss of load I don't have that
14 value.

15 MEMBER WALLIS: You sat in on the last
16 presentation?

17 MR. FREDERICK: Yes.

18 MEMBER WALLIS: Where I asked for a table
19 comparing before and after?

20 MR. FREDERICK: Again, we do have that for
21 all the limiting cases that we're talking about.

22 MEMBER WALLIS: It gives us some
23 perspective on what's going on.

24 MR. FREDERICK: Yes.

25 DR. BANERJEE: Loss of load may be ATWS

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1 and locked rotor, only of significance of right there,
2 the rest of them --

3 MEMBER SIEBER: ATWS is a service level D
4 event.

5 DR. BANERJEE: Yes.

6 MEMBER SIEBER: And loss of load is a
7 service level B event

8 MR. FREDERICK: That's correct.

9 MEMBER SIEBER: They're different limits,
10 right?

11 DR. BANERJEE: Yes, they have the same
12 pressure limits as well, right?

13 MEMBER SIEBER: Right.

14 MR. FREDERICK: Right.

15 DR. BANERJEE: But it would be interesting
16 to see what it was before.

17 MR. FREDERICK: What the results were
18 before?

19 DR. BANERJEE: Yes, compared to now. I
20 mean before and after.

21 MR. FREDERICK: Okay. I think we have
22 those. Do we have those, Chris, before?

23 MEMBER WALLIS: Yes. If they're not ready
24 this morning, you could flash them up this afternoon.

25 MR. McHUGH: Right.

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1 MR. FREDERICK: Yes.

2 MEMBER WALLIS: Now what limits your power
3 uprate? Is it secondary side or is it some of the
4 safety limits? Why don't you go to higher power
5 uprate? Is it safety limits that limit you?

6 MR. TESTA: This is Mike Testa again,
7 Beaver Valley.

8 When we first started the project and as
9 we showed in the beginning presentation, we looked at
10 where the industry was operating the Westinghouse 3
11 loop PWRs. And we basically are aligned with them. So
12 when we looked at the power level, we went to 2900
13 NSSS power, core power and that aligned us with the
14 other --

15 MEMBER WALLIS: So you looked at similar
16 plants and what they can do?

17 MR. TESTA: And then of course then we
18 looked at the modifications that we needed to perform
19 on the balance of plant side to achieve that.

20 MEMBER SIEBER: How much it --

21 MEMBER WALLIS: But conceivably if you've
22 gone to higher power, you might get a 2750 something
23 loss of load.

24 CHAIRMAN DENNING: Well, I have a relevant
25 question to that, and that is what -- it's not chance

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1 that the pressure has come to 2747/2746 right there.
2 Have you modified something like a setpoint or
3 something like that that brings you there? What is it
4 that --

5 MR. FREDERICK: Yes. One of the key inputs
6 to this analysis is the tech spec limit on the
7 tolerance for the setpoint for the safety valves. And
8 in the case of Unit 1 we increased that from one
9 percent to a three percent tolerance. And Unit 2
10 increased from 1 to 1.6. So it does drive the results
11 much closer to the limit. And we'll talk about that a
12 little later.

13 MEMBER WALLIS: You will talk about that?

14 MR. SENA: And this is Pete Sena, Director
15 of Engineer.

16 Again, Dr. Wallis, our goal here was to go
17 through the non-LOCA transients, take out the two most
18 limiting transients and then go into great detail so
19 you can see what margins do remain. That's what's Ken
20 is going to get to next.

21 MEMBER WALLIS: Thank you. That makes
22 sense. That's sort of thing we asked for last time.
23 So thank you.

24 MR. FREDERICK: This slide looks at some
25 of the other more unique criteria. Pressurizer filling

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1 is a concern essentially for progression. If we fill
2 the pressurizer, then the chances are we could evolve
3 into a small break LOCA which we don't want to happen.
4 So we look at that for some of the analysis which
5 challenged the overfill.

6 As you can see there, in the limiting case
7 the spurious SI, we do actually fill the pressurizer
8 and we'll have a more detailed discussion on that
9 event and what we've looked at to convince ourselves
10 that that's okay.

11 Margin to hot leg saturation or no boiling
12 in the hot leg is a criteria that's applied for
13 feedline break, which again is a condition IV event.
14 So this is a conservative criteria for that event.
15 And as you can see there, we have a margin to the hot
16 leg boiling.

17 MEMBER WALLIS: Loss of control you're
18 worried about, not popping something in the
19 pressurizer?

20 MR. FREDERICK: I'm sorry?

21 MEMBER WALLIS: The relief valve opens on
22 the pressurizer and then it fills up?

23 MR. FREDERICK: Yes. The concern there is
24 if you're passing water through a safety valve it's
25 not really designed for --

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1 MEMBER WALLIS: All right. But it can pass
2 with this water?

3 MR. FREDERICK: Yes.

4 MEMBER WALLIS: Right. But you lose
5 control, that's what you're worried about. You lose
6 pressure control?

7 MR. FREDERICK: Well, our concern would be
8 that the valve might stick open --

9 MEMBER WALLIS: It does happen.

10 MR. FREDERICK: -- which would reduce
11 pressure, yes. Yes.

12 MEMBER SIEBER: You have some other
13 problems, too. You have this huge water slug going
14 down the discharge line to the --

15 MR. FREDERICK: Yes, it would also
16 challenge the --

17 MEMBER SIEBER: -- to the PRT, which is
18 not a good thing.

19 MEMBER MAYNARD: You have separate power
20 operated type relief valves and code safeties?

21 MR. FREDERICK: Yes, we have power
22 operated relief valves as well as code safeties.

23 MEMBER MAYNARD: So the idea would be that
24 those would open up, use those before the code
25 safeties lifted, primarily?

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1 MR. FREDERICK: That's correct. Yes.

2 MEMBER MAYNARD: Yes.

3 MR. FREDERICK: The last even there shown
4 is the rod ejection where fuel stored energy limit the
5 acceptance criteria. And as shown there, we meet that
6 limit.

7 Next slide, please.

8 Again, this is a detailed discussion on
9 the loss of load event. Basically provide a flavor
10 for the level of conservatism --

11 MEMBER WALLIS: That BTU, what is that in
12 calories per gram.

13 CHAIRMAN DENNING: Calories per gram?

14 MR. FREDERICK: Pardon me?

15 MEMBER WALLIS: Usually it calories per
16 gram that we see. What is it?

17 CHAIRMAN DENNING: BTU per pound on max
18 fuel stored energy. Do you know what that is
19 conversion into calories per gram.

20 MR. FREDERICK: 260 or so.

21 MEMBER WALLIS: Or less?

22 MR. FREDERICK: Chris, if you want to look
23 it up, it's in the licensing report on that computer
24 there, I believe.

25 MEMBER WALLIS: Okay. We can do that.

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1 CHAIRMAN DENNING: We can probably handle
2 this conversion, but given half an hour.

3 DR. BANERJEE: And more oxygen.

4 MR. FREDERICK: Again, we're going to talk
5 about loss of load transients in detail here. And the
6 purpose is to give you an idea of the level of
7 conservatism that these analyses are done to.

8 And this event produces the highest
9 primary and secondary pressure of the condition II
10 events. And the results from either a loss of load
11 off the generator or a turbine trip that is caused by
12 other inputs.

13 The reactor protection for this event, we
14 have essentially five trips there that provide
15 protection. Two aren't credited; the high water level
16 trip and the pressurizer. That's just a conservatism
17 in the analysis. And the reactor trip on turbine trip
18 which is essentially the most direct trip for this
19 event, that's not credited because that is not
20 considered a qualified trip since it comes out of the
21 turbine building, which is a non-seismic building.

22 We do actually run two cases for this loss
23 of load, one to look at DNBR and one to look at the
24 pressure. We're not going to talk about the DNBR case
25 here. It's not close to being limiting.

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1 In the analysis we, of course, bias all
2 the input initial condition parameters to give us the
3 worst results. Initial pressurizer pressure and level
4 and the RCS power flow and temperatures; these are all
5 biased in the actual run as opposed to done separately
6 as we do for DNBR cases.

7 Also, we bias the reactivity feedback and
8 we use manual rod control for this analysis.

9 CHAIRMAN DENNING: These are all realistic
10 conditions, but it's just that you happened to pick
11 them all in combination in their worst --

12 MR. FREDERICK: That's correct. Their
13 initial control system setting, for example,
14 pressurizer level at 53 percent, 7 percent is added on
15 to that for uncertainty. So that's our initial
16 condition for this analysis.

17 We don't take any credit for any of the
18 control systems. Now essentially there's four control
19 system that would come into play here. You know,
20 condenser steam dumps. We also have atmospheric steam
21 dumps on the secondary side. On the primary side we
22 have pressurizer pressure control through the spray.
23 And we also have power operator relief valves which
24 would normally open up to 100 pounds below the code
25 safeties.

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1 For the code safety modeling we do use the
2 maximum setpoint allowed by the tech spec. In the
3 case of, for example, Unit 1 that is the setpoint plus
4 3 percent, which is our allowed tolerance or that
5 changes part of the EPU package.

6 Also in the valve modeling there's delays
7 model in the opening and that accounts for the time
8 that it takes to purge the water out of the loop seal.
9 In some cases, for example Unit 1 there's an opening
10 time associated with the valve. It's a target rock
11 valve. And there's also an additional shift put on
12 the setpoint based on the loop seal being present on
13 Unit 2.

14 The actual total impact of these changes
15 represents about a 200 pound increase above what they
16 would normally lift if we didn't include all these
17 conservatism.

18 Next slide.

19 This just gives you a very rough estimate
20 of the timing of the event. Essentially there's a
21 delay between the initial event and when the actual
22 trip begins of .5 seconds, which is very conservative
23 and then there's an additional two seconds before the
24 rods drop. And when the safety valves open is when we
25 get peak pressure, and that occurs at 8 seconds.

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1 And this plot basically just shows you the
2 pressure transient. Again, we're seeing from the
3 initial condition up to the peak it's about a 500
4 pound increase in pressure. And again, at 8 seconds
5 when the valve opened, the pressure drops.

6 DR. BANERJEE: What code was used, just
7 for my own?

8 MR. FREDERICK: LOFTRAN.

9 MEMBER WALLIS: Extraordinary accurate
10 code, as you can see.

11 DR. BANERJEE: Huh?

12 MEMBER WALLIS: Extraordinary accurate
13 code.

14 DR. BANERJEE: Right. Right. A
15 significant figure.

16 MR. FREDERICK: This slide shows you the
17 pre-EPU results. For Unit 1 that's a good comparison
18 because the same safety valve tolerance was used for
19 both cases, the 3 percent. So you see about a 15 pound
20 increase in the peak pressure associated with EPU.

21 On Unit 2 we actually lowered the
22 tolerance so actually you see the numbers dropping
23 there a pound or so.

24 If we do a more realistic analysis, and we
25 have, which credits control systems, we actually see

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1 a peak pressure much lower of about 2340 absolute. And
2 at that pressure we don't actually even lift any of
3 the safety valves on either side, primary or
4 secondary, or the pore for that matter.

5 If you go to the backup slide, and this is
6 a plot of that particular analysis both for pre-EPU
7 and EPU. And essentially they look identical. There
8 was no real impact of EPU in terms of the peak
9 pressure that we see in this analysis.

10 DR. BANERJEE: Well, why is that? What's
11 the physics?

12 MR. FREDERICK: Essentially the control
13 systems --

14 DR. BANERJEE: Safety valves are the same,
15 right?

16 MR. FREDERICK: Yes. And you're not even
17 opening safety valves here. So it's just a matter of
18 the control system acting the same and giving you the
19 same response out of the system.

20 DR. BANERJEE: But what does the control
21 system do here?

22 MR. FREDERICK: The control system opens
23 up the turbine bypass, the condenser steam dump
24 system. And that keeps the primary system from
25 heating much, I mean as much as you would normally

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1 see. And also --

2 DR. BANERJEE: Does it open the bypass
3 earlier or something just to shave the peak off? What
4 is happening? I'm trying to understand why the two are
5 so close to each other in spite of the fact that you
6 have 10 percent more power?

7 MR. FREDERICK: Right.

8 DR. BANERJEE: So what's the physics?

9 MR. FREDERICK: Yes. Well, the power
10 doesn't really enter into it much at this point. Yes,
11 it does cause a general heat up and so --

12 DR. BANERJEE: And that causes --

13 MEMBER SIEBER: That's small.

14 DR. BANERJEE: -- total pressure to peak?

15 MR. FREDERICK: Well, after the reactor
16 trip and then once the valves open, then it turns
17 around all these --

18 DR. BANERJEE: Do the valves open earlier
19 in the --

20 MR. SENA: Again, this is Pete Sena,
21 Director of Engineering.

22 I think the difference between the two
23 analysis is that the original analysis takes no credit
24 for any control systems so the steam dump systems do
25 not operate at all. And in the realistic analysis

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1 we've done here we are taking credit for the operation
2 of those systems.

3 DR. BANERJEE: So the pre-EPU doesn't take
4 credit for the --

5 MR. FREDERICK: Pete, he's asking --

6 DR. BANERJEE: All right. There has to be
7 a good reason?

8 MR. SENA: Well, the pre-EPU and the post-
9 EPU analysis use the same --

10 DR. BANERJEE: It's done differently?

11 MR. SENA: No, no. They use the same
12 modeling. Why don't you go back, Ken, for the pre and
13 post-EPU

14 DR. BANERJEE: Then the question is why
15 does it?

16 MEMBER WALLIS: I think because it's
17 controlled.

18 CHAIRMAN DENNING: It's controlled.

19 MEMBER WALLIS: It's because it's
20 controlled. It's the same.

21 DR. BANERJEE: Something opens earlier,
22 right?

23 CHAIRMAN DENNING: Or bigger or more.

24 DR. BANERJEE: Controlled means they have
25 to control the flow on a valve or something.

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1 MEMBER WALLIS: It might open more, the
2 control.

3 MEMBER SIEBER: It doesn't open more. I
4 think --

5 DR. BANERJEE: It might open earlier.

6 MEMBER SIEBER: -- the differences between
7 these two curves are so subtle that you really can't
8 pick them out.

9 MR. FREDERICK: Yes, I would say that they
10 are not exactly the same, but on here they look pretty
11 close.

12 MEMBER WALLIS: Because they look exactly
13 the same.

14 MR. FREDERICK: And, again, we haven't
15 changed the control system so we'd expect it to
16 operate.

17 DR. BANERJEE: Right. So what are the
18 control events here? Like what's happening?

19 MR. FREDERICK: You have the loss of load
20 times zero.

21 DR. BANERJEE: Right. And then there's
22 some trip?

23 MR. FREDERICK: And the reactor trips, in
24 this case on turbine trip but there's a 2 second delay
25 model.

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1 DR. BANERJEE: But both of them trip at
2 the same time?

3 MEMBER SIEBER: No.

4 DR. BANERJEE: Why not?

5 MR. FREDERICK: Well, the condenser steam
6 dumps this and responds to the trip signal. And also
7 it's based off of a delta T. Essential it looks at T_{avg}
8 and where T_{avg} should be post-trip, T_{ref} we call it.
9 And that delta drives the valve. So that program in
10 the system isn't changing, so it's essentially
11 maintaining the RCS conditions in a very similar
12 manner so you see a very similar result here.

13 MEMBER SIEBER: But the heat up is
14 slightly faster so the system operates slightly
15 quicker?

16 MR. FREDERICK: Yes. I mean it's a
17 proportional --

18 MEMBER SIEBER: I mean you could pick it
19 out here.

20 MR. FREDERICK: -- band. So if the system
21 demands more, the valves will open faster and more.

22 DR. BANERJEE: I know what you're saying
23 probably makes some sense, but what I'm really trying
24 to understand is when you show the curve, like this
25 curve here, this curve is the result of a very complex

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1 set of -- relatively complex set of control actions.

2 Now between the pre-EPU and the post --

3 MR. FREDERICK: That curve does not
4 actually use any of the control systems.

5 DR. BANERJEE: Okay. Take one which does.
6 Let's say --

7 MR. FREDERICK: This one does.

8 DR. BANERJEE: Yes, this one. So that
9 there are several control actions taking place. And
10 the fact that the two curves look so similar is
11 because there could be subtle differences. But the
12 fact they look so similar is due to control actions
13 taking place at different times in the two.

14 MEMBER SIEBER: Slightly different times.

15 MR. FREDERICK: The valves could be
16 opening faster because that's what they're programmed
17 to do.

18 DR. BANERJEE: Yes.

19 MR. FREDERICK: They look at an error
20 signal.

21 DR. BANERJEE: Well, whatever it is.

22 MR. FREDERICK: And if the error signal is
23 higher, than the values will open faster and further.

24 MEMBER SIEBER: And once they're open,
25 they're the same in the pattern.

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1 DR. BANERJEE: Ten percent more power is
2 produced in the other, right?

3 MR. FREDERICK: That's correct.

4 DR. BANERJEE: So it has to go somewhere?

5 MR. FREDERICK: That's correct.

6 MR. FREDERICK: So something must open
7 faster?

8 MEMBER SIEBER: Yes.

9 DR. BANERJEE: There's no other way.

10 MR. FREDERICK: Yes.

11 DR. BANERJEE: Right. Okay. So that's, I
12 guess, what doesn't come out clear.

13 MEMBER WALLIS: That's what turns things
14 around?

15 DR. BANERJEE: Yes. So what doesn't come
16 across is what are the actions which are turning
17 things around here? What's happening? So in one case
18 things are happening faster; that's why it's
19 happening.

20 MR. FREDERICK: Yes. The actions that are
21 occurring, again, the control system is trying to
22 drive T_{avg} down to the no load value, post-trip.

23 DR. BANERJEE: Right.

24 MR. FREDERICK: And the system responds
25 based on the delta. You know, where T_{avg} is versus

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1 where I want it to be. So if in the case of EPU that
2 delta is higher initially, then the valves will open
3 faster and further so that you would see the same type
4 of response --

5 MEMBER WALLIS: The system is actually
6 programmed to produce a curve like this?

7 MR. FREDERICK: That's correct.

8 MEMBER WALLIS: By control.

9 MR. FREDERICK: Yes.

10 MEMBER WALLIS: That's why the two curves
11 are the same.

12 MR. FREDERICK: Yes.

13 DR. BANERJEE: So what would be sort of
14 valuable to know is how much more rapidly do these
15 control actions have to occur in the second case. The
16 curves look the same but the control actions are
17 occurring faster or something is happening, otherwise
18 they wouldn't.

19 MR. FREDERICK: Right. Yes. I'd say it's
20 a very small difference. This whole peak occurs within
21 8 second.

22 DR. BANERJEE: One second makes a
23 difference, right, and 8 seconds --

24 MEMBER SIEBER: Yes, but it's 50 seconds
25 just for that first --

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1 MEMBER WALLIS: Depressurization.

2 MEMBER SIEBER: -- pressure peak and drop.

3

1 DR. BANERJEE: Yes. I wanted to know how
2 much.

3 MEMBER SIEBER: Yes.

4 DR. BANERJEE: In 8 seconds? Is it 6
5 seconds versus 8 seconds?

6 MEMBER SIEBER: It's hard to pick off that
7 graph.

8 DR. BANERJEE: Right.

9 MEMBER MAYNARD: Well, the rate is going
10 to depend on how much a discrepancy between --

11 MEMBER SIEBER: How big the delta is, yes.

12 MR. FREDERICK: Actually, just a couple of
13 weeks ago we had a loss of load event on Unit 2. And
14 we captured some of the data from that, the pressure
15 data.

16 MEMBER WALLIS: You arranged it to happen?

17 CHAIRMAN DENNING: Yes, you didn't do this
18 just for us?

19 MR. FREDERICK: No.

20 DR. BANERJEE: What's that slide number?

21 MR. FREDERICK: It's a backup slide. It's
22 not in your book.

23 DR. BANERJEE: This is one we must have,
24 right?

25 MR. FREDERICK: I'll get that for you.

1 MEMBER SIEBER: Ralph says he has it.

2 MR. FREDERICK: You see here again the
3 LOFTRAN prediction with the control cases. Generally
4 overall the modeling responds pretty well to the
5 actual event, the difference here being the initial
6 spike. And that's primarily because of the LOFTRAN
7 analysis assumes a 2 second delay from the time the
8 turbine trips until the reactor trips. And that's
9 what's making that. So in reality when we had this
10 event, we didn't see any pressure increase at all.

11 Just to give you an overall flavor, you
12 know, our safety analysis says that pressure is going
13 to go up 500 pounds. This is an actual event.

14 MEMBER WALLIS: The LOFTRAN can be off by
15 what? Quite a bit.

16 MEMBER SIEBER: Fifty pounds.

17 MEMBER WALLIS: Seventy pounds or
18 something?

19 MEMBER SIEBER: Fifty pounds.

20 MR. FREDERICK: We modeled the event
21 exactly as it happened. We were confident that we
22 would get very similar results.

23 DR. BANERJEE: No, no. But it's much
24 better you did it this way, really. Because if it
25 agreed too well, then we'd just think you tuned it.

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1 MR. FREDERICK: That ends my discussion on
2 loss of load. We're going to move on and talk about
3 rod withdrawal power unless there's any other
4 questions.

5 Again, the rod withdrawal power is the
6 limiting event in terms of the DNBR. And this event
7 can be initiated by either a malfunction in the rod
8 control system or an operator error.

9 As you can see, there's numerous reactor
10 protection trips.

11 MEMBER WALLIS: So how many rods are
12 withdrawn? How many rods are involved in this?

13 MR. FREDERICK: Is it one bank, Chris?

14 MEMBER WALLIS: One bank?

15 MR. McHUGH: We don't do it that way. We
16 do it by inserting reactivity into the core and we do
17 a range of reactivity insertion --

18 MEMBER WALLIS: Okay.

19 MR. McHUGH: -- from 110 pcm per second
20 all the way down to nearly nothing. We don't
21 explicitly model a certain number of rods. We model
22 it in terms of reactivity.

23 MR. FREDERICK: But that bounds
24 essentially one bank at maximum speed.

25 MR. McHUGH: Yes.

1 MEMBER WALLIS: Well, I'm just trying to
2 figure out what kind of operator error could produce
3 this. Is he limited to withdrawing one bank and so
4 on.

5 MEMBER SIEBER: Well, you're normally set
6 to withdraw or insert a bank at a time. But if
7 there's a malfunction or an error, it's probably going
8 to be one bank

9 MEMBER WALLIS: But an operator who had
10 some malfunction in his head, presumably withdraw a
11 lot of rods.

12 MEMBER SIEBER: I don't think he can do
13 that.

14 MEMBER WALLIS: He can't do that?

15 MEMBER SIEBER: He can pick out what bank.
16 You can circle all the rods.

17 MR. SENA: Again, this is Pete Sena.

18 For operator action, only one rod bank can
19 be withdrawn at a time unless you're in the overlap
20 region where two banks can be moving simultaneously.

21 MEMBER WALLIS: So you bounded what's
22 possible?

23 MR. SENA: That's correct.

24 MEMBER WALLIS: Yes.

25 MR. FREDERICK: Some of these trip

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1 functions also generate rod withdrawal blocks in the
2 system, but those are not credited as part of this
3 analysis.

4 As Chris mentioned, we do a range of
5 reactivity insertion rates and we also analyze this at
6 three distinct power levels, as shown there. In
7 total, there's about 90 cases that are run.

8 Again, this is a very conservative
9 analysis. Initial conditions are biased, again to
10 give us the worst case results in terms of DNBR.

11 MEMBER WALLIS: Now CHernobyl happened 20
12 years ago tomorrow. And I guess what they did was
13 they put a lot of reactivity into their reactor. A
14 tremendous amount.

15 CHAIRMAN DENNING: But not by rod
16 withdrawal.

17 MEMBER WALLIS: Not by rod withdrawal?

18 CHAIRMAN DENNING: No. No. They did it --

19 MEMBER KRESS: They did it by moderator.

20 CHAIRMAN DENNING: Moderator.

21 MEMBER KRESS: Negative coefficient. Not
22 moderator. Coolant.

23 MEMBER MAYNARD: Starting from a very low
24 power.

25 MEMBER KRESS: Yes, it was extremely low.

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1 MR. FREDERICK: Again, the conservative
2 values for trip functions as well as initial
3 conditions and reactivity feedback reviews. The
4 highest worth rod is actually assumed to be stuck out
5 of the core.

6 One thing to note is that at Beaver Valley
7 we have actually eliminated the capability to pull
8 rods in the automatic mod. So when our rod control
9 system is in automatic, the rods cannot be withdrawn.
10 So it just eliminates some potential for this event to
11 happen.

12 Slide, please.

13 Difficult to see here, I guess, but the
14 curve here basically shows you a plot of what the DNBR
15 result is versus the range of reactivity insertion
16 rates that we've analyzed for both minimum and maximum
17 feedback. Essentially you see the limiting case here,
18 the 1.57 result. We're actually at a very low
19 reactivity insertion rate. Essentially the lower
20 rates cause the system to respond slower so you tend
21 to get a worse result in that case.

22 The table shows the pre-EPU and the EPU
23 result. Essentially there was very insignificant
24 change in the result. Primarily that is due to the
25 fact that we've changed the correlation from the old

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1 correlation to the WRB-2M in which we gained some of
2 the margin. Again, that's associated with the real
3 effect of the RFA fuel and the intermediate flow
4 mixers. So essentially we gained a margin back that
5 the power uprate would have used here for this event
6 by changing the fuel pipe.

7 And again, I just want to mention that the
8 1.55 limit that's applied to this event and the other
9 ones, we also have 20 percent of margin in that limit.
10 So it's a conservative analysis and we have margin.

11 CHAIRMAN DENNING: Not to imply you have
12 the old fuel in there, but you've said before it's
13 something like a 20 percent effect on DNBR, the mixing
14 that's occurring there?

15 MR. FREDERICK: Yes.

16 CHAIRMAN DENNING: So that if you had done
17 the power uprate with old fuel, you would have had
18 something like 1.37 or is that over estimating what
19 the impact would be? Okay. Suppose you had done
20 power uprated but you had old fuel in there --

21 MR. FREDERICK: Right.

22 CHAIRMAN DENNING: -- would you have
23 gotten about a 1.37 here? Is that your assumption?

24 MR. FREDERICK: Chris, can we predict
25 that?

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1 MR. McHUGH: I can look that up. I think
2 we actually made those runs. Because we had planned
3 to do the power uprate before we had a complete
4 transition to RFA fuel. I believe I have that on my
5 laptop.

6 CHAIRMAN DENNING: Okay.

7 MR. McHUGH: We were going to limit
8 peaking factors on the burnt fuel, and so it wouldn't
9 have been a direct --

10 CHAIRMAN DENNING: There would have been
11 other things that could have done --

12 MR. McHUGH: Right.

13 CHAIRMAN DENNING: -- that it would have
14 reduced the --

15 MR. McHUGH: Correct.

16 DR. BANERJEE: Is it 20 percent
17 difference, the new fuel in rough terms?

18 MR. McHUGH: Twenty percent margin was
19 what they gained by adding the IFM grids to the RFA
20 fuel. So, yes, it was about a 20, 21 percent increase
21 in DNB margin from the old fuel to the new.

22 DR. BANERJEE: Magic.

23 CHAIRMAN DENNING: Magic.

24 MR. BURGER: Yes. If we were to have the
25 old B5H design in there, the peaking, like Chris said,

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1 would have been a lower limit that we do have, because
2 you don't have those IFMs and so they would have been
3 the limiting assembly in the core.

4 MEMBER WALLIS: And all good engineering
5 seems like magic to the layman.

6 DR. BANERJEE: I think Jeff Hewitt might
7 disagree on this one.

8 MR. FREDERICK: Okay. The next event that
9 we're going to talk about in some detail is the
10 spurious SI or invertent DCCS. Again, this is another
11 condition II event, which is initiated by either a
12 malfunction in the system which trips the SI signal or
13 perhaps some error in doing some testing of the
14 systems.

15 The SI or the safety injection signal will
16 generate a reactor trip and a subsequent turbine trip.
17 DNBR for this event really isn't challenged because
18 you're adding cold borated water into the system.

19 The primary concern here is filling the
20 pressurizer, which again can enlist the valves and
21 actually water through the safety valves.

22 Again, this is a very conservative
23 analysis and we have actually done better estimate
24 type analyses which show we do not overfill. But in
25 the conservative safety analysis we do fill the

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1 pressurizer and lift the safeties.

2 Now the conservatism that go into this
3 analysis, again, are primarily in the initial
4 pressurizer level again assumed to be setpoint plus
5 uncertainty at a high condition and also at the high
6 T_{avg} condition, which raises the level again.

7 The initial conditions in temperature and
8 flow are all biased for the worse results.

9 We actually run this with and without
10 pressurizer heaters, which is a control system but it
11 ends up effecting the temperature of the water, which
12 is one of the inputs into the valve operability
13 analysis. Colder water generally is worse for the
14 valves than hotter water.

15 Again, two high head pumps start, and
16 that's essentially what fills the system. For this
17 analysis the PORVs which normally would open and
18 prevent the safety valves from opening for this,
19 they're not credited essentially because they are a
20 control system.

21 One assumption that we also make in here
22 is that when cool water enters the pressurizer as it's
23 filling up, that water is assumed to mix
24 instantaneously with the bulk fluid where you would
25 expect some stratification normally. That, again,

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1 minimizes the temperature in the pressurizer and
2 that's an input into the value operability analysis
3 and it makes it more conservative.

4 Essentially this event ends when the
5 operator takes action to either open the PORVs or
6 shutdown and reset the SI signal and turn off the
7 pumps.

8 If you look at the next slide, the
9 assumption made here is that occurs at 10 minutes.
10 And we've done simulator studies to assure ourselves
11 that we can meet that limits.

12 MEMBER WALLIS: Isn't he watching his
13 pressurizer level all this time?

14 MR. FREDERICK: George, do you want to
15 speak to that?

16 MR. STORLIS: Yes. I'm George Storlis.
17 I represent Operations and my background has been
18 years of controlling Operations.

19 The pressurizer level is a key parameter
20 that's monitored and it's the duty of the licensed
21 operator at all times. And managing that level in the
22 crises of an inadvertent SI is of utmost importance.

23 The automatic features systems prevent the
24 manual shutdown for a period of time at the onset.
25 But the parameters are monitored. The procedures are

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1 detailed, emergency operating procedures are followed
2 and the termination of the flow rates when determined
3 not required are of immediate importance.

4 CHAIRMAN DENNING: What's your backup
5 slide here? Everything you took there, I get curious.

6 MEMBER WALLIS: Curious about it, huh?

7 MEMBER SIEBER: Sure do.

8 MR. FREDERICK: This is just plots from
9 the analysis results. We see here that a pressurizer
10 goes to its maximum level in about 7 minutes.

11 Next slide.

12 This shows the pressure as the safety
13 valve cycle opened and closed. In cycling, the number
14 of cycles is another important parameter that we need
15 for our valve analysis. And for this case you can see
16 we have five cycles of the valve before the operator
17 mitigates the event.

18 MEMBER SIEBER: And that's in a 100
19 seconds, roughly, 150 seconds?

20 MR. FREDERICK: That's correct. Yes.

21 DR. BANERJEE: Do you get any two phase
22 flow through these valves or is it just blowing steam?

23 MR. FREDERICK: Well, in this case the
24 pressurizer is full, so --

25 DR. BANERJEE: So you get water?

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1 MR. FREDERICK: -- a water discharge.

2 MEMBER WALLIS: But doesn't it flash when
3 it gets --

4 DR. BANERJEE: Yes.

5 MEMBER SIEBER: Yes, it does.

6 MR. FREDERICK: Yes. It flashes in the
7 discharge --

8 MEMBER WALLIS: Now there's indication of
9 temperature in the discharge line, isn't there, in the
10 control room? Probably rings a bell or something.
11 When there's a temperature in the discharge line from
12 the pressurizer it's measured, isn't it?

13 MR. FREDERICK: Yes. There is a tailpipe
14 alarm, yes.

15 MEMBER WALLIS: He's told. As soon as
16 this thing happens, he's told if he doesn't know
17 already.

18 MR. FREDERICK: Yes.

19 MEMBER SIEBER: You can assume that the
20 water in the pressurizer is saturated.

21 DR. BANERJEE: In which case it will get
22 critical fast.

23 MEMBER WALLIS: Critical flaw at pressure.
24 Right.

25 DR. BANERJEE: So do you use a critical

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1 flow calculation at that point once it comes out?

2 MR. FREDERICK: Chris, the safety valve
3 flow model, is that --

4 MR. McHUGH: I believe it's critical flow
5 -- the first cycle usually starts out with a little
6 bit of steam and then the pressurizer rapidly fills
7 once it opens and the remainder of the cycle is water.
8 And then the remaining cycles are typically all water.
9 The first one does start with steam typically.

10 MR. FREDERICK: This slide just shows how
11 the pressurizer water temperature drops as your
12 discharging water out of and it's insurging. And
13 again, it's assumed to instantly homogenize and reach
14 a bulk temperature.

15 DR. BANERJEE: Do you have a graph of the
16 discharge rate? I mean, how the discharge varies?
17 You showed a slide previously, I think that was --

18 MEMBER WALLIS: It seems to depressurize
19 very rapidly on that slide.

20 DR. BANERJEE: Yes.

21 MEMBER WALLIS: There seems to be plenty
22 of flow there.

23 MR. FREDERICK: The mass flow rate out of
24 the valve, is that what you're asking?

25 MEMBER WALLIS: Yes.

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1 DR. BANERJEE: It must be very high.

2 MR. FREDERICK: Yes, it is.

3 MR. MCHUGH: I think I have that
4 information on my laptop.

5 MEMBER SIEBER: So you're solid, there's
6 no cushioning effect from any steam in there. So the
7 pressure is going to go up very rapidly.

8 DR. BANERJEE: Can I see the previous
9 slide, please?

10 MEMBER WALLIS: See how rapidly it comes
11 down?

12 MEMBER SIEBER: Again, because you're
13 solid.

14 DR. BANERJEE: Yes. You don't have to do
15 it now, but if you've got it on your laptop, nice to
16 see it.

17 MR. FREDERICK: Chris, it's in the RAI
18 responses that we submitted, so --

19 DR. BANERJEE: Is it?

20 MR. FREDERICK: Yes.

21 DR. BANERJEE: The 3,000 pages or
22 something, no?

23 MR. FREDERICK: So, again, yes this
24 analysis does generate overfill of the pressurizer and
25 as such, the results are essentially used as inputs to

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1 an evaluation that we do to determine whether or not
2 the safety valves are going to function under the
3 conditions that we're presenting to them.

4 The valve evaluation uses WCAP 11677
5 methodology. And that's primarily based on results
6 from the EPRI valve testing that was done post-TMI
7 where they actually put water through the valves at
8 various conditions and temperatures.

9 The PORVs are also qualified. We looked
10 at those in terms of water discharge as well as the
11 discharge piping on both the PORVs and the safety
12 valves. We've analyzed all the lines for these
13 conditions and shown that we met the limits.

14 MEMBER WALLIS: Because you can get
15 choking in the discharge line. Can get critical flow
16 in the discharge line because the depressurization is
17 tremendous.

18 MR. FREDERICK: Yes. Was it a RELAP
19 analysis to generate the forcing functions on that,
20 Mike?>

21 DR. BANERJEE: Yes, you can get multiple
22 choking in lines like this, but RELAP wouldn't
23 calculate that, I would think.

24 MEMBER SIEBER: Yes. There's a number of
25 elbows in that line. I think the analysis that was

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1 done was to make sure that the line would stay intact.
2 There's tremendous forces on that line as this slug of
3 water goes --

4 MEMBER WALLIS: Well, if it chokes at the
5 discharge into the drain tank, that's where you worry
6 because then you get a pressurization of the whole
7 line.

8 MEMBER SIEBER: Yes. Well, I would imagine
9 almost immediately the drain tank ruptured just with--

10 MEMBER WALLIS: No. There is a while,
11 isn't there, before that happens?

12 MEMBER SIEBER: Pardon?

13 MEMBER WALLIS: Isn't there quite a while
14 before that happens?

15 MR. TESTA: Yes. This is Mike Testa.

16 We analyzed the piping from the
17 pressurizer from the pressurizer itself and including
18 the piping down to the PRT. And as Ken said, you know
19 once we overfill, of course, and we're putting water
20 down the line, we used the RELAP computer code to
21 derive the forcing functions. And then incoded that
22 into the piping analysis, piping model to make sure
23 that the piping and the supports would remain intact
24 or acceptable.

25 MEMBER WALLIS: You don't challenge the

1 rupture disk of the drain tank?

2 MR. TESTA: No, I don't believe we did.

3 MEMBER SIEBER: To what, 50 pounds?

4 CHAIRMAN DENNING: We're running behind,
5 but that's okay. We're going to let this go.

6 MEMBER WALLIS: You mean we may be a
7 little late tonight?

8 CHAIRMAN DENNING: Exactly.

9 MR. FREDERICK: I just have one more area
10 before --

11 CHAIRMAN DENNING: That's okay.

12 MEMBER WALLIS: Are you going to do large
13 break LOCA before you --

14 MR. FREDERICK: Yes.

15 CHAIRMAN DENNING: Yes.

16 MR. FREDERICK: One other issue which the
17 Staff raised on the concern here was if the PORVs
18 opened, they wanted us to demonstrate that we had a
19 qualified signal for them to close, even though the
20 PORVs are considered a control grade. However, they
21 do have a signal which comes out of the protection
22 grid systems which close the valves on a low pressure
23 signal from the pressurizer. So the concern here was
24 if you needed to rely on block valves which would be
25 available then that was more of a condition III, that

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1 we were able to demonstrate that we do have a
2 qualified signal to close the valves.

3 So summary on the spurious SI, we have analyzed
4 the valves for the water discharge condition was
5 identified and we're convinced the valves can pass
6 water without damage. Likewise, for the PORVs and the
7 PORVs do have the qualified signal to close. And this
8 event will not promulgate a condition III event.

9 MR. SENA: Again, this is Pete Sena.

10 I just want to also reemphasize a couple
11 of things.

12 Jack, you asked about the PRT, the
13 ruptured disk goes at a 100 pounds, not 50 pounds. And
14 additionally, we've simulator crews both units through
15 an inadvertent SI scenario. And they are able to
16 diagnose the event, confirm that we do not have the
17 actual real event such as a LOCA or a tube rupture,
18 and terminate the SI prior to going to solid
19 conditions. And actually, in 2002 we had a real
20 inadvertent SI on Unit 1. And based on that real
21 plant data we also did go solid in that case.

22 CHAIRMAN DENNING: What was the nature of
23 the event that occurred? How did it --

24 MR. SENA: What happened in 2002 at Unit
25 1, one of our main steam isolation valves closed due

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1 to a human performance error involving the building of
2 scaffolding. The closure of that valve then resulted
3 in a low steamline pressure from the other two steam
4 generators supplying the turbine. So again, you do
5 not have a valid steamline break, but that's what it
6 sensed at 500 pounds low steamline pressure. So a
7 safety injection signal was actuated and a reactor
8 trip from full power.

9 CHAIRMAN DENNING: Two high pressure
10 points?

11 MR. SENA: Yes, two high pressure safety
12 injection pumps actuated, all ECCS pumps actuated.
13 Operators were able to progress through the EOPs and
14 terminate the SI prior to going solid.

15 MR. FREDERICK: Just to wrap the non-LOCA
16 discussion here. Again, for the analyses that we've
17 done we've shown that we meet all the DNBR limits as
18 well as the pressure limits for primary and secondary.
19 And all the acceptance criteria for the condition II,
20 III and IV events are met at the EPU conditions.

21 Again, that's it for the non-LOCA and
22 we'll move on to large break LOCA unless there's any
23 questions on that.

24 For EPU we have, again, gone to the best
25 estimate LOCA methodology, as we discussed before.

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1 And, again, this is the original 1996 approved
2 methodology that Westinghouse has used for many
3 plants.

4 Due to the methodology, there is some
5 benefit in terms of the PCT result as well as changes
6 that were made in the containment and accumulator
7 minimum pressure, which also provides some benefit in
8 terms of the PCT. The container pressure associated
9 with conversion increases the initial operating
10 pressure about 4 psi. And that increase in the back
11 pressure transient that associated with the LOCA event
12 does provide a benefit in terms of PCT. And primarily,
13 this is due to a reduction in what we call downcomer
14 boiling. The downcomer boiling tends to impede vessel
15 refill and that is very sensitive to the containment
16 back pressure.

17 Also we did primarily for small break
18 analysis we raised the minimum accumulator pressure
19 and that had a small benefit here as well.

20 So essentially some of the margin that we
21 would lose from EPU we have regained by some of the
22 other plant changes that we've made.

23 And the results, as shown on the next
24 slide here --

25 DR. BANERJEE: What is the small slide?

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1 MR. FREDERICK: Okay. This is a general
2 discussion about what DE methodology is. If you're
3 interested, we can talk about it.

4 MEMBER WALLIS: No. They're conservative
5 assumptions, all of these things.

6 MR. FREDERICK: Yes. This basically goes
7 through what assumptions are bounding and then the
8 balance that I talked about how the uncertainties were
9 rolled into the final PCT value.

10 MEMBER WALLIS: A response surface type of
11 thing, is it?

12 MR. FREDERICK: That methodology, yes, it
13 does use the response surface.

14 MEMBER WALLIS: Now what surprised me
15 here, maybe I'm ignorant of these, it looks as if
16 you're limited by your maximum hydrogen generation.
17 Usually the peak clad temperature that limits. And
18 you seem to have an awful lot of oxidation in yours.

19 MR. FREDERICK: In the BELOCA methodology
20 is --

21 MEMBER WALLIS: Is it because it stays hot
22 for a long time or something, is that what it is?

23 MR. FREDERICK: Pardon me?

24 MEMBER WALLIS: Why are the oxidation
25 numbers pushing the limit? Usually it's the peak clad

1 temperature. Is it because --

2 MR. FREDERICK: For the hydrogen
3 generation.

4 MEMBER WALLIS: -- the temperature stays
5 high for a long time or something?

6 MR. FREDERICK: Right. Matt, do you want
7 to address that in terms of the conservatism?

8 MEMBER WALLIS: A bit strange to me.

9 MR. CERRONE: Yes. This is Matt Cerrone
10 with Westinghouse.

11 Well, first of all, you're right. They do
12 have an extended reflood period so they have a higher
13 PCT and you can see this manifests itself in the core
14 wide oxidation number.

15 In the methodology, the development of
16 that number is conservative. It's very conservative
17 in that the transient used to generate the numbers
18 developed based on PCTs that are beyond the 9th
19 percentile and it has -- the transient goes for a
20 longer period of time than the PCT transient.

21 So basically what you're doing is you're
22 making sure that you have a high transient that has a
23 high PCT and has an extended reflood period. Okay.

24 And then beyond that, the local
25 uncertainty code that we use extends the reflood heat

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1 transfer longer in time. So basically it's a
2 conservative number. And the methodology allows for
3 additional COBRA/TRAC calculations to be performed as
4 a measure to reduce the additional -- reduce the
5 conservatism until ultimately you show success at the
6 hydrogen generation, 1 percent acceptance criterion.

7 Three's an additional work that could be
8 performed to show additional margin in that number.

9 MR. FREDERICK: Yes. I guess the answer
10 there is we do enough to show we meet the limit and we
11 don't push it beyond that, although there are
12 additional margin to be gained.

13 MEMBER WALLIS: But the question for
14 Westinghouse, is this an unusual plant where the CWO,
15 the core wide oxidation seems to be the limit here?
16 It doesn't seem to be in my memory a very common
17 thing.

18 MR. CERRONE: Well, no, it's not all that
19 common, certainly.

20 MEMBER WALLIS: Is there something unusual
21 about this plant or the method of analysis, or what?

22 MR. CERRONE: No. It's not unusual. The
23 evaluation techniques were in line with what was in
24 the approved evaluation model. So I think here we're
25 just seeing a PCT and a high oxidation, a higher

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1 oxidation number. But like I had said additional work
2 could be performed if it was so needed to generate
3 additional margin and the maximum hydrogen generation
4 number.

5 DR. BANERJEE: Are you going to show us
6 some curves or clad temperature with times so we get
7 a feel for what's going on?

8 MR. FREDERICK: I did not include those,
9 no for the large break. I do have some for small
10 break.

11 DR. BANERJEE: So it would help, I think,
12 in answering some of these questions to see how long
13 the fuel clad temperature remained high or whatever
14 and when reflood came in.

15 MR. FREDERICK: Matt, do we have the
16 BELOCA WCAPS here?

17 MR. CERRONE: Yes, I brought Unit 1 and
18 Unit 2 reports with me.

19 MR. FREDERICK: Okay. Well, the technical
20 reports do have that information if you want to look
21 at it.

22 DR. BANERJEE: Yes. We don't need all the
23 details, but at least a few for the temperature
24 transient. And they can show it later, maybe.

25 MR. CERRONE: I could check to see if am

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1 electronically, if not I have I think a reference
2 transient with the one break would show an
3 illustration.

4 MR. FREDERICK: Yes. Just make some copies
5 of those graphs.

6 DR. BANERJEE: Right.

7 MR. FREDERICK: And then you can pass them
8 out.

9 DR. BANERJEE: Of the relevant graphs.

10 MR. FREDERICK: Right.

11 CHAIRMAN DENNING: And we could do that
12 during lunchtime and then look at them after lunch if
13 we want to take a look at that.

14 MR. FREDERICK: So essentially a PCT
15 transient --

16 MR. CERRONE: OF the large LOCA.

17 MR. FREDERICK: For the large LOCA.

18 CHAIRMAN DENNING: Yes. I think
19 particularly --- yes. You'd like to see also if you
20 can in what time period is the hydrogen being
21 generated. Over what time period --

22 MEMBER WALLIS: Right. Right.

23 CHAIRMAN DENNING: -- is hydrogen
24 generation occurring.

25 MR. CERRONE: It'll help illustrate that.

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1 I mean, the time at the transient is above 1700 degree
2 is when you'll be oxidizing.

3 MR. CARUSO: The transient, though, that
4 you're going to show us is that necessarily the one
5 that produces the maximum hydrogen generation?

6 MR. CERRONE: No.

7 MR. CARUSO: That's a problem. Because
8 you probably don't have the graph that generates
9 maximum hydrogen generation. So --

10 MEMBER WALLIS: It's not the same as the
11 PCT graph.

12 MR. CARUSO: It's not the same as the PCT.

13 MR. CERRONE: For each period; blowdown,
14 early reflood and late reflood. A PCT at the 95th
15 percentile is developed in this methodology. In the
16 95 EM an additional COBRA/TRAC transient's computed
17 where the PCT calculated goes beyond that of the 95th
18 for each of the three periods. So what you do them is
19 you capture the oxidation period above the 95th
20 percentile with the COBRA/TRAC calculation. So you
21 oxidize above the temperatures all experienced in each
22 period at the 95th percentile and you capture the time
23 and temperature.

24 MR. CARUSO: Is that the scenario you're
25 going to present to us?

1 MR. CERRONE: Well, I was just thinking
2 through that. The engineering report, I do not
3 believe, provides the oxidation transient that was
4 developed.

5 MR. CARUSO: That's what I was wondering.

6 MR. FREDERICK: Yes, I think it will be
7 somewhat representative.

8 MR. CARUSO: Okay.

9 MR. FREDERICK: Kind of a general --

10 MR. CARUSO: Because you just have to be
11 careful, Sanjoy. I think you're looking for the
12 actual transient that generates that .98 percent and
13 you're not going to see that. You're going to see
14 something similar.

15 MR. CERRONE: Yes. I think what we can do
16 is take each time period --

17 DR. BANERJEE: The reason, of course, is
18 that what -- at least the way you're putting it, it's
19 a very conservative calculation, right?

20 MR. CERRONE: Correct.

21 DR. BANERJEE: Maybe we need to have that
22 when you show -- well, the first thing it would be
23 nice to get the curve which produces that .98, which
24 is relatively close to the limit, right?

25 The second is that the conservatism maybe

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1 should be just listed as a snapshot for us to see so
2 that we can say okay, that .98 is really an upper
3 limit, I mean it's very conservative or something like
4 that. Did I come across? I mean, do you have a feel
5 for it?

6 MEMBER WALLIS: Because we're discussing
7 a power uprate and it hasn't changed tremendously from
8 .91.

9 DR. BANERJEE: Right. That was pretty
10 high already.

11 MEMBER WALLIS: Yes, that as pretty high
12 already.

13 DR. BANERJEE: It went from a very
14 conservative calculation of .91 to a best estimate of
15 .98?s

16 MR. CERRONE: Well, we need to keep in
17 mind that the oxidation calculation is conservative
18 even in the original '96 evaluation model using
19 COBRA/TRAC. And keep in mind also that additional
20 COBRA/TRAC calculations could be performed at various
21 power levels to capture the rod power senses
22 throughout the core to give you more and more -- to
23 give you additional levels of margin. The idea is
24 that there's a regulatory limit that we must comply
25 with. And we basically provide a sufficient amount of

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1 evidence that we've met that limit.

2 DR. BANERJEE: Yes. I guess when you say
3 best estimate here, you really have markings in this
4 best estimate.

5 MEMBER WALLIS: Yes. It's not totally best
6 estimate..

7 DR. BANERJEE: Yes.

8 MEMBER WALLIS: There's a lot of
9 conservatism on top of it.

10 MR. CERRONE: Yes. Especially in the
11 oxidation calculation. We look forward to the ASTRUM,
12 when we move to ASTRUM with this because there is
13 oxidation margin.

14 DR. BANERJEE: Perhaps that could be at
15 least clarified. Because I'm confused.

16 MEMBER WALLIS: Well, I think the best
17 estimate number would be much lower if you went from
18 the mean rather this 95th percentile in that.

19 MR. CERRONE: I would agree.

20 MEMBER SIEBER: The difficulty, though, is
21 in regulatory space you either meet the number or you
22 don't.

23 MEMBER WALLIS: That's right. That's
24 right.

25 MEMBER SIEBER: And the conservatism you

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1 have --

2 MEMBER WALLIS: And you do have enough to
3 do that. Right. Right.

4 MR. CERRONE: There's always been plenty
5 of ways to find margin --

6 MEMBER WALLIS: That's why it came out to
7 .98 because you had to be under one.

8 MR. CERRONE: Sure. I mean you did a
9 sufficient number of calculations, you show
10 compliance.

11 MEMBER WALLIS: That's right. I
12 understand.

13 DR. BANERJEE: Anyway, we want listing the
14 assumptions and conservatism with that curve, then at
15 least we have a feel for it.

16 CHAIRMAN DENNING: Okay. I think we can
17 proceed.

18 MR. FREDERICK: Okay. Yes, we're done
19 after this one.

20 The one thing I wanted to point out here
21 was that the P-clad temperature that you see there for
22 Unit 1 will be a different number as even the draft
23 SER. When we did the original Unit 1 analysis the
24 result came out to 2144. And those original analyses
25 were based on different containment operating

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1 conditions that we had in place at the time or we're
2 proposing for the containment conversion. When we
3 changed those initial conditions, we went back and
4 reanalyzed both units. And the number for Unit 1
5 dropped primarily because we lowered our peaking
6 factor limits associated with Unit 1 analysis because
7 we were seeing an unacceptable increase due to the
8 containment pressure change. So that's the result
9 that we will be reporting essentially is official
10 50.46 type results is the 21 number.

11 DR. BANERJEE: What is the reason for the
12 different between Unit 1 and Unit 2?

13 MR. FREDERICK: In the results?

14 DR. BANERJEE: Yes.

15 MR. FREDERICK: The major difference
16 between the plants is in the downcomer area. One unit
17 has what they call thermal shields and the other one
18 has the neutron blanket. And those represent,
19 basically, fairly significant thermal masses but they
20 are different between the plants. So Unit 2 tends to
21 be a lot less sensitive to downcomer boiling type
22 conditions, low pressure in containment than Unit 1.

23 Initially actually Unit 1 resolve was
24 actually much higher, was 2144 for similar input
25 conditions. For example, the peaking factors were

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1 originally all the same. The result here is that
2 they're not that different here, but actually Unit 1
3 here is restricted to a lower peaking factor limit
4 than 2. The difference in the plant is reflected
5 in the analysis.

6 DR. BANERJEE: Raising of the containment
7 pressure didn't take care of this downcomer boiling
8 problem?

9 MR. FREDERICK: It helps, but it does not
10 completely eliminate.

11 That's all I had on large break. I guess
12 we're going to shift over to the NRC now.

13 CHAIRMAN DENNING: Yes. We'll at least
14 start the Staff's presentation here and then we'll see
15 if we want to have a breaking point in the middle of
16 it, if that's okay.

17 MR. MIRANDA: Okay. The answer to your
18 first question is we're using this overhead projector
19 because I have some transparencies with some transient
20 plots on there and I'd like to have the ability to
21 draw on them.

22 My name is Sam --

23 MEMBER WALLIS: On the screen, whatever
24 you do.

25 DR. BANERJEE: Well maybe draw on the

1 screen so we can have it changed and focused.

2 MEMBER SIEBER: We already tried that.

3 MR. MIRANDA: My name is Sam Miranda. I
4 work at the PWR Systems Branch of NRR as a technical
5 reviewer.

6 I've been with the NRC for a little more
7 than 5 years. And before that time I worked for
8 Westinghouse as a nuclear safety analyst for almost 25
9 years, during which time I used LOFTRAN code and
10 worked with the author of LOFTRAN, Toby Burnett to
11 write several routines in LOFTRAN.

12 First I will go quickly through the --

13 DR. BANERJEE: Where are these slides?

14 MEMBER SIEBER: They're in here, I think.
15 I'm going blind.

16 MEMBER WALLIS: That's almost as good as
17 the other one.

18 MR. MIRANDA: Okay. For the EPU at Beaver
19 Valley there is no change in the fuel design. By the
20 time the EPU will be implemented, the entire core will
21 be composed of robust fuel assemblies. And there's
22 been no change in the methodology used for the nuclear
23 design.

24 As far as thermal hydraulics is concerned,
25 since the entire core is robust fuel assemblies,

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1 there's no DNBR penalty for the fuel transition. And
2 the THINC IV code has been replaced by the VIPRE code
3 in the DNBR evaluations.

4 Both --

5 DR. BANERJEE: The difference between
6 these codes?

7 MR. MIRANDA: The VIPRE code seems to be
8 more flexible. You can model cores with, for example,
9 hexagonal lattices rather than just square lattices.
10 There are features in VIPRE that allow it to do things
11 that THINC has problems doing.

12 DR. BANERJEE: Are these subchannel codes
13 or what?

14 MR. MIRANDA: They're detailed core models
15 where you can have a hot channel and you can have
16 surrounding fuel assemblies and you can also model the
17 fuel itself, the pellet, the gap and the clad,
18 calculate temperatures and stresses and heat flux.

19 Both the revised thermal design procedure
20 and the standard design procedures were used in the
21 analyses depending upon the limits of these methods
22 and the requirements of the accident analyses
23 themselves, as discussed earlier by Mr. Frederick.

24 This is a review of the large break LOCA
25 analyses and as compared to the 10 CFR 50.46 limits.

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1 CHAIRMAN DENNING: And you're showing the
2 older version of the peak clad temperature for Beaver
3 Valley 1?

4 MR. MIRANDA: The older version?

5 CHAIRMAN DENNING: That's not 2144
6 anymore.

7 MEMBER SIEBER: Yes, that's one cycle
8 before the cycle --

9 MR. MIRANDA: Revised.

10 MR. FREDERICK: Ken Frederick.

11 That is the value that we had on our
12 original analysis before we reanalyzed.

13 MR. MIRANDA: Yes. We didn't incorporate
14 the new number in this slide, but yes the licensee has
15 submitted a new number.

16 MEMBER WALLIS: This is something that we
17 don't have, this slide, is that right?

18 DR. BANERJEE: Do we have this slide?

19 MR. MIRANDA: No, you don't have this
20 slide. This was added at the last minute.

21 CHAIRMAN DENNING: So you'll get us a copy
22 of this. Okay. But there's nothing new on there?

23 MR. MIRANDA: No.

24 CHAIRMAN DENNING: Stick it up just
25 another second. That's basically just supposed to show

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1 us what the applicant calculated.

2 MR. MIRANDA: Right.

3 CHAIRMAN DENNING: Right. And we've
4 already seen that.

5 MR. MIRANDA: And to show you that the
6 limited have been met, yes.

7 CHAIRMAN DENNING: Okay. Good. Thanks.

8 MR. MIRANDA: I'm going to get into a
9 discussion here about the margins and acceptance
10 criteria and then which will lead into a discussion of
11 the results for three examples of transient analyses.
12 And this is going to be very basic.

13 We have on the left hand column the ANSI
14 criterion that defines conditions I, II, III and IV
15 events and the acceptance criteria and how we get from
16 there to the analysis criteria.

17 The ANSI standard from 1973 defines
18 anticipated transients condition II events, otherwise
19 known as anticipated operational occurrences. As
20 events that could occur during the calendar year of
21 operation at a plant. And it's defined basically as an
22 event that basically requires no more than a reactor
23 trip. Plant trips you correct a condition and you're
24 back to power in short order.

25 There are basically three analysis

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1 criteria that apply to condition II events. One is
2 that the RCS does not overpressurize and also the main
3 steam system does not overpressurize. Another is that
4 you have no fuel clad damage, and this demonstrated by
5 showing that you meet the DNBR safety analysis limit.
6 And finally, that the condition II event does not
7 develop into a more serious event. And this criterion
8 is designed to prevent a shortcut or short circuit in
9 the sense that you can't have a condition III or IV
10 event that originates as a condition II event with a
11 condition II frequency of occurrence. Because a
12 condition III or IV event has other acceptance
13 criteria.

14 And as far as analyses are concerned, this
15 last condition that the event does not promulgate into
16 a more serious event is shown by demonstrating through
17 analyses that the pressurizer doesn't fill. And this
18 is done to preclude the possibility of passing water
19 through any of the pressurizer relief or safety valves
20 which may not be qualified for water relief. And in
21 deterministic accident analysis if a valve is not
22 qualified for water relief, it's assumed to stick
23 upon. And a stuck open valve then constitutes a small
24 break LOCA in the steam space of the pressurizer.

25 Another option to satisfy this criterion

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1 is to qualify the valves in question, either the
2 pullers or the safeties or both. And in this case
3 Beaver Valley is qualified to safety valves.

4 Condition III events which may occur
5 during the lifetime of the plant, there is some
6 allowance for fuel clad damage. And these are
7 governed mainly by the dose consequences which have to
8 meet the 10 CFR 20 release limits. But in many cases
9 in accident analyses this is satisfied merely by
10 meeting the more stringent condition II criteria.

11 As far as condition IV events are
12 concerned, the limiting faults also dose criteria
13 apply, 10 CFR Part 100. And, again, a lot of the
14 accident analyses, steamline break is one example,
15 where this is satisfied by meeting the condition II
16 criteria.

17 There's also 10 CFR 50.46 with the PCT
18 limits and so on. And that's all aimed at the ANSI
19 standard from 1973 which talks about maintaining the
20 ability of protection systems that are needed to
21 mitigate the event. And that goes to the -- of the
22 core and maintaining core geometry.

23 In accident analyses found in Chapter 15
24 the non-LOCA events, this is often shown by showing
25 that there's no boiling in the RCS system and no hot

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1 leg saturation. And this happens to be a Westinghouse
2 internal criterion. By showing that there's no
3 boiling in the RCS, you can show that the core will
4 not uncover and the event ends there. The evaluation
5 need not continue to more complicated factors. It
6 also happens, it's very convenient for Westinghouse
7 since LOFTRAN is not capable of modeling a two phased
8 flow. So when you reach a hot leg saturation you
9 should be done with that analysis.

10 There's another category here they added,
11 ATWS. ATWS is not covered by this ANSI standard.
12 ATWS was invented in 1969 by an ACRS consultant named
13 Dr. Epler. And the Staff issued guidelines for
14 analysis of that ATWS and acceptance criteria in WASH-
15 1270. And ATWS was the first category that was to be
16 analyzed according to a probabilistic safety goal of
17 no core damage. I believe it was something like 10 to
18 the minus 5, then it went to 10 to the minus 7, then
19 it went back to 10 to the minus 6. But the various
20 vendors submitted analyses in 1974 to show the
21 consequences of ATWS. And this issue continued until
22 the promulgation of the ATWS rule in 1986, 10 CFR
23 50.62 which actually does not require analyses. It
24 just requires the installation of certain hardware.

25 For PWRs this is a diverse SCRAM system

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1 and an ATWS mitigation systems actuation circuitry.
2 And for Westinghouse plants it's just the AMSAC
3 system, because Westinghouse demonstrated that DSS was
4 not justified.

5 ATWS analyses are conducted on a best
6 estimate basis. And the principal criterion there is
7 RCS overpressurization. And the level C stress limit
8 was chosen as the acceptance criteria, 3200 psig. And
9 this is based on review of the various components of
10 the RCS system and picking the weakest component. In
11 many cases that is the reactor coolant pump cases.

12 And another item that's important in this
13 level C stress limit is the valve disks for valves
14 that are needed to proceed to safe shutdown. The
15 pressure has to be kept to a level such that there
16 would be no deformation of the valve disks so that
17 they remain operable and the plant can proceed to safe
18 shutdown after a ATWS.

19 This is similar to what you've seen
20 before. This example, which is based on the WRB-2M
21 correlation shows that the correlation limit, the 95
22 percentile ability, the 95 percent confidence level is
23 1.14. And this includes uncertainties that are
24 encountered during the development of the correlation.

25 And then the design limit 1.22 includes

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1 the operational uncertainties on power level,
2 temperatures and flow rate mainly.

3 And then to this is added some margin.
4 For Beaver Valley's case it's about 21 percent. And
5 this margin would include, for example, transition
6 core DNBR penalty, would include rod bow. In this
7 case, the transition core, the DNBR penalty doesn't
8 apply.

9 For the reactor coolant pressure boundary,
10 I've chosen the level C stress limit, I'll call that
11 the best estimate since it's used for ATWS analyses.
12 And then the safety analysis limit is the 110 percent
13 of design pressure, which leaves us a margin of about
14 17 percent.

15 CHAIRMAN DENNING: One second. On the
16 1.55, Staff has accepted lower values than 1.55 for
17 these kinds of transients, is that true on a CHF?

18 MR. MIRANDA: Yes. Yes. That's true.

19 CHAIRMAN DENNING: This is a reasonably
20 conservative value from your interpretation?

21 MR. MIRANDA: Yes. Yes, it's reasonable.
22 I've actually compared to other plants, this has more
23 margin.

24 CHAIRMAN DENNING: Thank you.

25 MR. MIRANDA: Now I'm going to talk a

1 little bit about margins and where they're found. And
2 in the first grouping is in the acceptance criteria
3 themselves. And from a prior slide we saw that the
4 analysis criteria are more stringent, there's more
5 margin in there in order to show that the standard
6 acceptance criteria met. The standard acceptance
7 criteria sometimes can be a little bit hard to
8 measure, but the analysis criteria have to be
9 measurable.

10 So in the acceptance criteria themselves,
11 some events are analyzed according to more stringent
12 criteria. For example, the steamline break, a
13 condition IV event, or the complete loss of flow, a
14 condition III event, are both analyzed according to
15 condition II acceptance criteria meaning no clad
16 damage.

17 Then there's also some margin between the
18 acceptance criteria and the standard in terms of
19 shortcuts like the pressurizer no fill criterion. And
20 also as far as the fraction failed fuel rods. And the
21 condition III and IV event, for condition IV events
22 for example, the fraction of failed fuel rods is
23 largely determined by the dose consequences. And the
24 fraction of failed fuel rods some value is chosen that
25 is known to produce acceptable dose consequences. In

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1 a prime reading for Ginna, for example, there was a
2 statement in the Ginna SE which talked about the
3 assumed level of failed fuel rods. This refers to the
4 practice of doing an analysis, doing a rod census and
5 calculating the number of rod failure. And if it
6 meets some predetermined level, for example, 10
7 percent, then it's acceptable. Very often that number
8 is much less than that, maybe 2 or 3 percent. The 10
9 percent value would be used by the dose people as
10 standard practice. Get the dose consequences for a 10
11 percent level of fuel rod failures when the analysis
12 actually shows something much less.

13 In the initial conditions and parameter
14 values, the initial conditions for the accident
15 analysis are taken in the conservative direction.
16 Power level, for example, would be at 102 percent
17 power. RCS temperatures depending upon the accident
18 analysis and what they are looking for, very often the
19 RCS temperature would be about 4 degrees higher than
20 nominal. There's also some level of steam generator
21 tube plugging that's assumed as well as pressurizer
22 and steam generator water levels.

23 The protection system setpoints are also
24 taken in the conservative direction.

25 MEMBER WALLIS: This is what's done by

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1 this plant. It's not always done, is it?

2 MR. MIRANDA: It's always done, yes.

3 MEMBER WALLIS: Always done?

4 MR. MIRANDA: Always done.

5 MEMBER WALLIS: Even in a best estimate
6 with uncertainty, you still have these conservatism?

7 MR. MIRANDA: Well, these are not best
8 estimate analyses. These are conservative analyses.

9 MEMBER WALLIS: Conservative?

10 MR. MIRANDA: Yes.

11 In practice, taking all of these
12 uncertainties in the conservative direction could
13 actually wind up with a plant in a configuration
14 that's not possible physically, but they do it anyway.
15 You might, for example, take the under block values
16 for core reactivity and beginning of life values for
17 temperatures.

18 Core reactivity feedback, for example.
19 They might take a most negative moderator temperature
20 coefficient which would occur at end of life, it might
21 be much more negative than actually expected. And
22 then at beginning of life you would have a zero
23 coefficient or positive coefficient. The object there
24 is not only conservatism, but also to produce a very
25 wide range of analyzed space so that in the future for

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1 core reloads of different core designs with different
2 core moderator temperature coefficients and other
3 coefficients, doppler for example, if those values for
4 the characteristic of the core reload fall within this
5 range, that would tend to eliminate the need for new
6 analyses.

7 And Westinghouse calls this their reload
8 safety evaluation checklist.

9 There's also margin added to key parameter
10 values used in the accident's analyses. Rod drop
11 time, for example, was typically 2.8 seconds. The
12 actual value is closer to 1½ seconds. Safety
13 injection flow if it's conservative to have a minimum
14 flow of, then the pump, the performance codes are
15 taken at a minimum value.

16 Decay heat generation is another example.
17 Decay heat generation --

18 MEMBER WALLIS: Is this stuff in a Reg.
19 Guide somewhere or is it actually in the rule, or is
20 it just the way it's done?

21 MR. MIRANDA: This is the practice. Yes.

22 MEMBER WALLIS: This is precedent. It's
23 not rule?

24 MR. MIRANDA: No. It's experience.

25 MEMBER WALLIS: This is the way it's

1 normally done?

2 MR. MIRANDA: Yes. Yes.

3 Decay heat generation is another one I'm
4 sure you're familiar with. It's either 1971 model plus
5 20 percent or a 1979 model plus 2 sigma.

6 And Scram worth, typically for a
7 Westinghouse plant that might be 4 percent. The actual
8 value is closer to 6 percent because they assume that
9 the most reactive rod is stuck out of the core.

10 Just in response times. The same thing.
11 Typically rods don't get begin to drop until maybe 2
12 seconds after the signal was received. And that actual
13 value is closer to 1 second or .8 seconds

14 Also response times in terms of pump
15 startup times to reach full speed or opening valves.
16 For example in the safety injection system before flow
17 delivery could occur to the RCS, it might be 10
18 seconds. It's actually less than that, especially if
19 you consider for example the relationship between flow
20 area and valve position.

21 MEMBER WALLIS: All of this sounds
22 qualitatively good. But until you put it in a terms
23 of a probability distribution or something, I don't
24 really know what you're gaining. I mean you say we're
25 going to assume 2 seconds when reality is more like 1.

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1 But presumably it's one with some uncertainty.

2 MR. MIRANDA: Yes.

3 MEMBER WALLIS: Your two is somewhere way
4 beyond the uncertainty bound or it's sort of 99.9999
5 percentile or something, or what is it? It sounds
6 good, but I don't have an idea.

7 MEMBER SIEBER: You do rod drop tests and
8 I think two is the ultimate limit, but most of the
9 time a rod will drop around 1 second or 1.2 seconds.

10 MEMBER WALLIS: That's a qualitative
11 statement.

12 It all sounds good, but I just wonder why
13 it isn't all put into some soundness, sort of
14 probabilistic basis and then we can do a bounding
15 best estimate with uncertainty.

16 MR. MIRANDA: This method predates PRA.

17 MEMBER WALLIS: Yes, it does. It seems to
18 be a bit archaic. That's why you're using this
19 particular projector, isn't it?

20 MR. MIRANDA: It's consistent, yes.

21 MEMBER SIEBER: It's structural.

22 DR. BANERJEE: But it actually focuses
23 better.

24 MEMBER WALLIS: The focus is much better,
25 right.

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1 MEMBER SIEBER: Structuralist.

2 MEMBER WALLIS: It's cheaper to do it this
3 way?

4 DR. BANERJEE: Sounds like these are sort
5 of limiting values that you use?

6 MEMBER SIEBER: Yes.

7 MEMBER WALLIS: They are.

8 DR. BANERJEE: One end of the probability
9 distribution?

10 MR. MIRANDA: That's right. It is possible
11 sometimes to do sensitivity studies where you isolate
12 some of these things and you might do the same
13 analysis, for example, with a 2.8 second drop time and
14 a 1 second drop time and see what effect it has on
15 your parameter of interest. And you can do this for
16 hundreds and hundreds of cases and come up with some
17 kind of a relationship. But it hasn't been necessary
18 as long as you show that the safety analysis limit is
19 met, there's no point in going any further.

20 DR. BANERJEE: And maybe you don't know
21 the probability distributions anyway, you know.

22 MEMBER MAYNARD: Right.

23 MR. CARUSO: That costs money to determine
24 that.

25 MR. MIRANDA: Well, okay.

1 MEMBER SIEBER: Well, from a legal
2 standpoint this method is much easier to defend; you
3 either make it or you don't. You build a box and the
4 reactor fits in there, it's good. If it doesn't fit in
5 there, it's not good.

6 MR. CARUSO: And if you have a problem
7 meeting your criteria at some point, then you go look
8 at an individual factor and say, well, is it necessary
9 for me to refine that value in order to meet the
10 criteria. And then you have to develop the data
11 that's needed to support the value that you use. But
12 it's easier to use the limiting value until you need
13 to.

14 MEMBER SIEBER: That's the old regulatory
15 system. And it is still used pretty widely.

16 MEMBER WALLIS: It produces the same
17 results on Monday as it does on Tuesday.

18 MEMBER SIEBER: That's great.

19 MEMBER WALLIS: Well, is an interesting --

20 MEMBER SIEBER: And Plant A and Plant B
21 look the same if they are the same.

22 MR. MIRANDA: There' margin also in the
23 methods used in the analyses. We heard a little bit
24 earlier about critical flow through the pressurizer
25 safety valves. LOFTRAN has several critical flow

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1 correlations in it and you use the appropriate model.

2 For example, steamline break you might
3 want a very high flow through the break.

4 For a case where you're worried about RCS
5 overpressurization and you're looking at flow through
6 the pressurizer safety valves, you might use a flow
7 correlation that produces a lower flow.

8 And it has, for example, homogeneous
9 equilibrium subcooled and saturated models, and moody
10 models.

11 Again, for steamline break make an
12 assumption that the steam break flow is dry steam.
13 This maximizes the cool down that the steam break
14 produces in the core and maximizes the core reactivity
15 response.

16 In actuality, a steamline break would have
17 considerable entrainment in it. And I know this from
18 experience because Turkey Point Unit 3 had a steamline
19 break in 1971 when they were doing pre-startup
20 testing. The core was not loaded at the time, but
21 they blew a safety valve off the header on the
22 steamline and the steam generator blew dry in a time
23 that was much faster than predicted by the computer
24 code. And the difference was attributed to water
25 entrainment.

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1 DR. BANERJEE: But I guess conservative
2 here must be carefully defined, right? It's
3 conservative with regard to some specific parameter
4 that is of concern, like peak clad temperature,
5 reactivity or whatever.

6 MR. MIRANDA: That's right. We'll see some
7 examples of that in the plots.

8 There's also as far as --

9 MEMBER WALLIS: What you're describing is
10 just what these guys did at Beaver Valley?

11 MR. MIRANDA: Yes.

12 MEMBER SIEBER: Yes.

13 MR. MIRANDA: Yes. This is standard
14 Westinghouse methods.

15 MEMBER WALLIS: I thought Westinghouse had
16 better methods now.

17 DR. BANERJEE: Well, only when they need
18 it.

19 MEMBER SIEBER: The answer is no? This is
20 the licensing approach.

21 MR. MIRANDA: Yes. This is methodology
22 that the Staff has seen before, it's familiar with and
23 has approved of.

24 LOFTRAN and RETRAN, but in this case we're
25 talking about LOFTRAN has a derivative method. They

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1 call it to estimate the DNB ratio. And this is a
2 shortcut.

3 Rather than go through the VIPRE analysis
4 to actually calculate a DNB ratio, LOFTRAN has the
5 results of sensitivity studies of the effect on DNB
6 ratio due to changes in pressure and temperature. And
7 during a transient, as you move through the transient
8 and you change temperature and pressure, it calculates
9 a DNB ratio. And this deliberately programmed into
10 LOFTRAN to give you a lower than expected DNB ratio.
11 And then the practice is depending upon what the DNB
12 ratio is. For example, if you do a raw hydraulic
13 power analysis, then you come up with a DNB ratio of
14 1.5 and the safety analysis limit is 1.55. You know
15 that 1.5 of value is conservative from LOFTRAN but you
16 can't prove it. So you take some stake points from
17 the analysis and you put them through a VIPRE analysis
18 and you come up with a better DNB ratio. And that's
19 very often much higher, 1.6, 1.65, whatever. But it
20 does eliminate a lot of VIPRE analyses to go through
21 this estimate.

22 MEMBER WALLIS: I believe this is all
23 going back to the days when it was expensive to use a
24 computer?

25 MR. MIRANDA: Yes. It goes back to those

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1 days. And furthermore, not only was it expensive to
2 use the computer, but you had to use several codes.

3 MEMBER WALLIS: Took a long time to run,
4 too, I think.

5 MR. MIRANDA: Took a long time to run. And
6 you had to physically take those stake points and put
7 them into another --

8 MEMBER WALLIS: Take some perforated paper
9 from one computer to another, or something.

10 MEMBER SIEBER: And boxes of cards.

11 DR. BANERJEE: Boxes of cards.

12 MR. MIRANDA: Yes. Yes. And a technician
13 with a piece of graph paper.

14 MEMBER SIEBER: Yes.

15 MEMBER WALLIS: Now are we back in the
16 '60s or something here? This is very interesting.

17 MR. MIRANDA: Yes. Actually we're in the
18 '70s.

19 MEMBER WALLIS: Back in the '60s.

20 MEMBER SIEBER: No, that's 1970s
21 technology.

22 MEMBER WALLIS: We should all feel really
23 young and full of energy, right?

24 MR. MIRANDA: LOFTRAN was written in 1970
25 and was in full use for licensing analysis by 1971.

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1 LOFTRAN is an abbreviation for loss of flow transient
2 and it was written to do the loss of flow transient
3 analysis for the Zorita Plant in Spain, a one loop
4 plant.

5 As far as transient assumptions are
6 concerned, the worse single act of failure in the
7 protection system is assumed, and this goes to the
8 IEEE 279 requirements 279 requirements. And then
9 again, the scram worth is based on the most reactive
10 rod stuck outside the core.

11 And we heard a little bit about this
12 earlier, about no credit for operation of control
13 grade systems. And typically these are the
14 pressurizer PORVs, heaters and spray. And such systems
15 are assumed not to be operating in a transient unless
16 their operation would tend to make the transient
17 worse.

18 Sometimes you'll see in a set of accident
19 analyses several cases performed with and without the
20 operation of the control grade system to see the
21 effect.

22 And then there are some trips that are
23 just not taken credit for. And the example of the
24 reactor trip on turbine trip was alluded to earlier.
25 And also the rods don't fall into the core when

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1 offsite power is lost. The rods fall into the core
2 only after reactor trip signal is received.

3 I can discuss, by the way, before I get
4 into the transients, if you're interested I could talk
5 a little bit about the overtemperature delta T trip
6 and how that's determined.

7 At this point I'll go to the conclusions.
8 The bottom line, very simple, when we look at an
9 analysis, for example the DNBR limit. If the minimum
10 calculated DNBR from the transient is greater than the
11 safety analysis limit, then the analysis is
12 acceptable.

13 If the minimum calculated DNBR should
14 equal the safety analysis limit, then the analysis is
15 still acceptable because we know that we have margin
16 in both the limit and in the accident analysis.

17 And if the minimum calculated DNBR should
18 fall below the safety analysis limit, now we can't
19 accept the analysis because it hasn't been
20 demonstrated that there's adequate margin still
21 available. There's obviously been some erosion of
22 that margin and we have no idea of how much is
23 remaining. And this goes back to what you said, Dr.
24 Wallis. We don't have that relationship between the
25 best estimate value and the uncertainty.

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1 MEMBER WALLIS: Now when the licensee
2 calculates these numbers, he's not able to tweak his
3 code to make it less than or more than? We all know
4 that by changing nodalization and time steps and all
5 sorts of things you can tweak codes to get different
6 results. He's not allowed to tweak his code? How do
7 you prevent him from just dialing a lot of tweaks and
8 eventually getting within the regulations?

9 MR. MIRANDA: Well, we can't prevent him
10 from doing that. And if the modeling has been
11 accepted; an acceptable model should not be very
12 sensitive to things like time steps and nodalization
13 for a non-LOCA analysis.

14 DR. BANERJEE: They generally are, that's
15 the problem. I mean, essentially all these finite
16 difference code depend on nodal volumes and time
17 steps. They're not mathematically convert in any sense
18 of the word. They're too nonlinear. There's also
19 some weird things in them.

20 MEMBER WALLIS: Like the business of
21 matching the currant number at one and not somewhere
22 else, and therefore getting distortion there.

23 MR. MIRANDA: You can tweak the code a
24 little bit, but only a little bit with LOFTRAN because
25 LOFTRAN is not like a LOCA model. It's a hard wired

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1 simulation. It has a pressurizer. It has steam
2 generators. And you have very little leeway as far as
3 nodalization is concerned. You can put three nodes in
4 the hot leg or you can put 20 nodes in the hot leg;
5 the results should not be that much different.

6 The same thing with the core. You can put
7 several nodes axially and radially in the core but, it
8 won't have that much of a difference.

9 MEMBER WALLIS: That's why we've always
10 said that the Staff should have the ability to run
11 these codes itself. Find out how sensitive they are to
12 these various things rather than just taking something
13 submitted by the licensee, who has obviously optimized
14 things to make it look good.

15 MR. MIRANDA: As a matter of --

16 MEMBER WALLIS: Or he has the chance to do
17 that, let's say. But you don't have these
18 Westinghouse codes run by the Staff, do you?

19 MR. MIRANDA: Well, for Beaver Valley and
20 Ginna we do have use of the LOFTRAN code. We have
21 access to the LOFTRAN code through Westinghouse's
22 office in Rockville. And we have the LOFTRAN manual
23 and we have the safety analysis standards.

24 MEMBER WALLIS: When they report a number
25 like, whatever it is, 2748.5 when it should be 2750,

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1 you can run your own LOFTRAN or whatever it is and
2 figure out if you can get it to 2502.1 or something?

3 MR. MIRANDA: We could, yes.

4 MEMBER WALLIS: 2750.3 or whatever it is.

5 MR. MIRANDA: Yes. Yes. We could change
6 a few parameters --

7 MEMBER WALLIS: You have a really good
8 idea of how much tweaking they could do to get what
9 they want?

10 MR. MIRANDA: I've done this tweaking
11 myself.

12 MEMBER WALLIS: That's it, you're an
13 insider.

14 MR. MIRANDA: There isn't that much you
15 can do. You might be able to change the result by a
16 couple of psi, but unless you make some basic changes
17 in the assumptions. You would need, for example you
18 would need to change the critical flow model that
19 you're using. And making changes like that require
20 justification. You need to have a reason for doing
21 that.

22 MEMBER WALLIS: It really takes a Staff
23 member who has done this stuff him or herself to be
24 able to understand what the licensee is doing or what
25 Westinghouse is doing. Otherwise you can be

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1 bamboozled.

2 DR. BANERJEE: Or have an equal
3 capability, which is not LOFTRAN, which is in your
4 hands.

5 MEMBER WALLIS: Like TRAC?

6 DR. BANERJEE: Whatever, yes.

7 MEMBER SIEBER: Yes. Well, LOFTRAN is only
8 one code. There's a lot of codes that are used here.

9 DR. BANERJEE: Yes.

10 MEMBER SIEBER: There are VIPRE, MAAP.

11 DR. BANERJEE: At least to keep them
12 honest to do a few spot checks here and there.

13 MR. MIRANDA: Yes. And we have done a
14 couple of those.

15 MEMBER SIEBER: They do audit. You do
16 audits?

17 MR. MIRANDA: Yes. We did an audit for
18 Beaver Valley in November of last year, three days at
19 Westinghouse's offices in Pittsburgh where we looked
20 at the --

21 MEMBER WALLIS: When are we going to take
22 a break?

23 MR. MIRANDA: -- analyses, we looked at
24 the calculation notes behind the analysis and also the
25 safety analysis standards. And we talked to the

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1 people who performed these analyses.

2 CHAIRMAN DENNING: Sam, let me interrupt
3 you at this point. I think this is a good breaking
4 point, would you not agree?

5 MR. MIRANDA: Sure.

6 CHAIRMAN DENNING: Well in that case,
7 we're going to adjourned then until by that clock 25
8 after 1:00.

9 (Whereupon, at 12:30 p.m. the meeting was
10 adjourned, to reconvene this same day at 1:30 p.m.)
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A-F-T-E-R-N-O-O-N S-E-S-S-I-O-N

1:30 p.m.

CHAIRMAN DENNING: Okay. We are now back in session.

And, Sam, you can start anytime you want.

MR. MIRANDA: Okay. I will step through three example of non-LOCA transients. And we have the same three transients that Beaver Valley was talking about earlier.

The first is a loss of external load. And this is the event that causes a very high reactor coolant system pressure. And followed by the rapid draw of power for the channels to DNB. And finally the spurious actuation of ECCS. And this event is the one that we look at in order to show that the event will not progress to a condition III or IV event.

The first event, the loss of external load I might comes in several varieties. There is a condition I loss of external load, an operational transient which is also known as a load rejection. We can reduce load by 50 percent and show that the plant will not trip.

There's also a loss of load ATWS, which is the limiting ATWS event in terms of pressure which will reach pressures very close to the 3200 psi limit.

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1 The loss of external load, and moving to
2 the earlier discussion, the best estimate case that
3 showed there was no difference between pre-EPI and
4 post-EPU, I might add that in that instance if you
5 have a loss of load and you have the steam dumping
6 available, basically that amounts to a 60 percent loss
7 of load. Steam dumping to the condenser will take up
8 about 40 percent of nominal steam flow. So comparing
9 that to an accident analysis loss of load, a 100
10 percent load rejection, there's a big benefit there;
11 first of all. And secondly, if you use the pressure
12 control system pulls and spray the spray will be
13 working during that event. So that seeing two curves
14 that are identical is not a surprise because here you
15 only have a 60 percent load rejection and you have
16 pressure being controlled by the sprays. And that is
17 very likely to be more than enough to handle the 8
18 percent power increase.

19 So for this event there are two cases
20 analyzed. I'm going to talk about both of them and
21 you'll see why in a few minutes.

22 The first case we have a case that's
23 analyzed for channels to the DNB. And in that case as
24 expected the overtemperature delta T trip is reached.
25 And the minimum DNBR occurs shortly after the rods

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1 begin to drop.

2 Typically the minimum DNBR will occur even
3 before the rods reach of the bottom of the core. When
4 most of activity has been inserted, transient is
5 already -- DNB ratio begins to increase again.

6 One thing I would look for in as a
7 reviewer in a case like this would be for a reactor
8 trip that comes from the part of the reactor
9 protection system that is designed to protect against
10 a parameter of interest. In this case we're worried
11 about DNB and the reactor protection system function
12 that protects against DNB is overtemperature delta T.
13 So if I saw a trip occurring from another source that
14 is not related to DNB, I would have questions.

15 So here we have the overtemperature delta
16 T trip operational.

17 The second case is the case that challenge
18 the RCS pressure limit. So here we have the nuclear
19 power and heat flux. Then I have drawn on this the
20 time of the reactor trip right here. And you'll see
21 that the nuclear power begins to drop quite soon. Heat
22 flux begins to drop just a little bit later. And
23 that's just due to the thermo-lag heat flux through
24 the fuel.

25 And this is the pressure and pressurizer

1 volume.

2 MEMBER WALLIS: Now it peaks out at the
3 flat top because it actually blows a relief valve, the
4 pressurizer?

5 MR. MIRANDA: This is the answer to your
6 question right there.

7 MEMBER WALLIS: Okay. That's it. Thank
8 you.

9 MR. MIRANDA: Now this is an example of
10 conservatism in the setpoints. The pressurizer safety
11 values are set to open nominally at 2500 psia with a
12 tolerance of plus or minus 3 percent. This is Beaver
13 Valley 1. And in this case since they are looking for
14 a low DNB ratio, they're want to keep the pressure
15 low. Therefore, they're using the low setting on the
16 pressurizer safety valves, opening them at 24, 25
17 psia, nominal minus 3 percent.

18 They're also using pressure control.
19 Pressurizer spray and pressurizer power operator
20 relief valves. So you see the first plateau is when
21 the relief valves open at 2350 psi and a second
22 plateau is when the safety valves open. Both of those
23 serve to keep the pressure low and keep the DNB ratio
24 low.

25 And then finally as a verification that

1 this is not an event that could proceed to a more
2 serious event, we see that the pressurizer does not
3 fill.

4 MEMBER WALLIS: Where is full pressurizer?

5 MR. MIRANDA: It's about 1428 cubic feet.
6 1420 cubic feet for the pressurizer and another 28
7 cubic feet for the surge line.

8 CHAIRMAN DENNING: Now, in this case if
9 they had the valves opening later, would it have
10 threatened the pressurizer more filling the
11 pressurizer?

12 MR. MIRANDA: If the valves were opening
13 later --

14 MEMBER WALLIS: It's not turned around by
15 the valves.

16 MR. MIRANDA: No, actually if the valves
17 opened earlier, the pressurizer level might be higher
18 because you're squeezing the steam out.

19 This is the last of that transient. This
20 mainly shows that the reactor coolant system pressure
21 here, this is the value that comes very close to the
22 2750 psi limit. And this is higher than the
23 pressurizer pressure because this pressure is measured
24 at the reactor coolant pump discharge. It's the
25 highest pressure in the system

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1 MR. CARUSO: Do we have that one?

2 CHAIRMAN DENNING: I don't think we do.

3 MR. MIRANDA: No. No, I just added that
4 just to show this. I don't think you have any of the
5 curves, do you?

6 MEMBER KRESS: Yes.

7 MR. MIRANDA: Okay. I just added that.

8 And then finally we have the parameter of
9 interest, the DNB ratio to show that it doesn't reach
10 the safety analysis limit. The limit is 1.55. This
11 is the same curve that the reactor trip noted there.
12 And you see that the reactor trip and the minimum DNB
13 ration are related. The reactor trip is what
14 mitigates this event. This is the classic definition
15 of a condition II event. All it takes is a reactor
16 trip.

17 Now we have another case without pressure
18 control. This is a case that's designed to maximize
19 the reactor coolant system pressure. And this will
20 have a higher pressure than the previous case. It's
21 still within the limit.

22 A similar behavior, there's the reactor
23 trip and the response in nuclear flux and heat flux.
24 And this occurred you saw earlier today was the peak
25 reactor -- here's a peak pressurizer pressure. And

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1 then you come down, on the way down, you see there's
2 a little plateau here. This is at 2575 psia

3 MEMBER WALLIS: It doesn't look right.
4 Oh, yes it does. It's okay.

5 MR. MIRANDA: 2575 --

6 MEMBER WALLIS: Yes, it's okay.

7 MR. MIRANDA: -- that is nominal subpoint
8 for the pressurizer safety valve.

9 MEMBER WALLIS: Around the peak. There's
10 a very sharp peak there.

11 MR. MIRANDA: Oh, that's the reactor trip.

12 MEMBER WALLIS: The reactor trip is what
13 cuts if off at 2700 or something. That's the way you
14 want to avoid. It just trips in time, doesn't it?

15 MR. MIRANDA: Yes. Yes. That's right.

16 MR. FREDERICK: This is Ken Frederick.

17 Actually, what we've seen is that when the
18 valves open is where we reach the peak. We actually
19 ran an additional case where we didn't credit the
20 first trip, we credited the second trip. And that
21 trip actually occurred after the peak. And the peak
22 was pretty much the same but it occurs right when the
23 valves open.

24 MEMBER WALLIS: So it's a valve opening
25 that causes the peak?

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1 MR. MIRANDA: Well, the valve opening
2 helps. In fact, this 2575 here, that's when the valve
3 begin to reseal. And that's the higher -- that's the
4 nominal setpoint plus 3 percent. Because the object
5 here is to maximize pressure. So they're using the
6 higher setpoint for the safety valves. And also in
7 this case we see that the pressurizer doesn't fill.

8 This is another curve that you don't have.
9 This is the reactor coolant system pressure to show
10 the maximum value. That's the number that you saw
11 earlier, the 2747 psia.

12 We can skip this one.

13 MEMBER WALLIS: So you're making FENOC's
14 presentation for them here?

15 MR. MIRANDA: Excuse me?

16 MEMBER WALLIS: This is all their results,
17 right?

18 MR. MIRANDA: Their results, yes.

19 MEMBER WALLIS: And so you're just showing
20 that you understand them? There's nothing that you
21 did to calculate anything separately?

22 MR. MIRANDA: Actually, I did --

23 MEMBER SIEBER: He probably do it.

24 MR. MIRANDA: I did the analysis that Mr.
25 Frederick was referring to.

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1 MEMBER WALLIS: Oh, you did the analysis
2 that they're using now?

3 MR. MIRANDA: No, no, no no. The one
4 where they took the second trip, I verified the
5 LOFTRAN ran.

6 MEMBER WALLIS: Okay.

7 MR. MIRANDA: That is designed to show
8 that these valve sizing meets the ASME design
9 criteria. That's according to Section 5.2.2 in the
10 FSAR.

11 Any questions on the loss of load?

12 As I said, the loss of load there's a
13 different of different variation. We've already
14 referred to four variations. The accident analysis,
15 the condition I event which could be a load rejection
16 anywhere from 40, 50, 60 percent, the ATWS analysis;
17 that's three variations.

18 Okay. Rod withdrawal with power. Rod
19 withdrawal with power is actually a series of
20 transient analyses that could be -- let's see, close
21 to a 100 different analyses that are performed. I'm
22 going to talk about two example.

23 One, at full power and 80 PCM reactivity
24 insertion rate, a high reactivity insertion rate and
25 another one at full power with a very slow reactivity

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1 insertion rate.

2 And these two events show that the high
3 neutron flux trip will protect against a high
4 insertion rate and the overtemperature delta T trip
5 will protect against very slow insertion rates.

6 There are other trips that come in, but
7 these are the ones that we look for in a rod
8 withdrawing power since these are directly related to
9 the event.

10 Here's the high reactivity insertion rate.
11 And we see we get the high flux trip. And there's
12 about a half a second delay and the rods begin to
13 fall. And as the rods fall, you can see the power
14 dropping. This is a very short time scale. It's only
15 7 seconds.

16 And since this is a condition II event,
17 they're also in addition for looking for the DNB ratio
18 limit, we're also making sure that the pressurizer
19 doesn't fill. In this case there's lot of margin to
20 filling.

21 DR. BANERJEE: What is the water volume
22 for filling the pressurizer?

23 MR. MIRANDA: 1400 cubic feet plus another
24 28 cubic feet for the surge line.

25 So the DNBR safety analysis limit is 1.55

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1 and this particular case the ADPC per second
2 reactivity insertion rate at full power meets the
3 limit.

4 And then for the slow reactivity insertion
5 rate, you can see this is a much longer transient. We
6 have about 2 minutes represented here. And the trip
7 comes from the overtemperature delta T trip. And this
8 event, by the way, is crucial to determining the
9 setpoints for the overtemperature delta T trip.

10 And in this case we see that the
11 pressurizer power operator relief valves opened right
12 here. But the pressurizer is still not full.

13 And here's the DNB ratio. And in this
14 case we come closer to the limit. I think that might
15 be the 1.57 case. DNB ratio is reached soon after the
16 -- while the rods are falling into the core.

17 And those are two cases, as I said, of
18 many more, possibly up to a 100. And the results of
19 all these cases are plotted in something like this.

20 As I said earlier, the cases that have a
21 very high reactivity insertion rate along here are
22 protected by the high flux trip. And the cases that
23 have slow reactivity insertion rates are protected by
24 the overtemperature delta-T trip. And actually these
25 curves continue. I think they go like this. Okay.

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1 But this plot shows that it was protected through this
2 very wide range of reactivity insertion rates, wider
3 than you might expect during operation by these trips,
4 the overtemperature delta T and the high neutron flux.

5 And I have more results along those lines.
6 This is at 60 percent power. And then at 10 percent
7 power.

8 That's the rod withdrawal of power
9 analysis. Any questions on that?

10 Okay. These DNB ratios, by the way, that
11 you see here are calculated by LOFTRAN, not by VIPRE.
12 And they used that derivative estimation method.

13 Now the next event, the spurious actuation
14 of safety injection at power is probably the only
15 event in Chapter 15 that actually challenges that
16 criterion that prohibits escalation of a condition II
17 event into a more serious event, at least that's the
18 only one we know of. And the mechanism is that you
19 have a spurious SI signal, a fairly common event, a
20 condition II event and causing the safety injection
21 system to actuate. And in some plants, like Beaver
22 Valley, the safety injection system includes the
23 charging pumps. And the charging pumps are capable of
24 pumping into the RCS at nominal pressure. In fact,
25 their shut off head is at 2600 psi. So they can not

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1 only can they pump into the RCS nominal pressure, they
2 can lift safety valves.

3 If they fill the pressurizer and lift out
4 of the PORVs or the safety valves, then the question
5 is if these valves are not qualified for water relief,
6 the deterministic accident analysis methods assume
7 that such valves once opened would stick open. And
8 that would be a condition III event, a small break
9 LOCA.

10 Beaver Valley is a little bit unusual
11 compared to other Westinghouse plants. Beaver Valley
12 has three PORVs rather than two.

13 Another interesting aspect of this
14 accident is that it's misunderstood, it has been
15 misunderstood in terms of its analysis. I've seen
16 analyses in licensing basis that talk about DNB ratio
17 and how DNB ration safety analysis is met. Even some
18 analyses that talk about RCS pressurization or
19 overpressurization. Neither is of concern.

20 First of all, the safety injection signal
21 will automatically trip the reactor that's in the
22 protection system. The reactor trips immediately. So
23 there's no danger of DNB.

24 And secondly, since the shut off head of
25 the charging pumps is only 2600 psi, there is no

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1 danger of exceeding 110 percent of design pressure.

2 So those two concerns go away and we're
3 left with the escalation to a condition II event.

4 So this illustrates how the graphic trip
5 occurs immediately. And we have the core temperature,
6 core average temperature dropping and then eventually
7 coming up to this level here. This is about 563. And
8 basically what this temperature is determined by the
9 secondary side temperature.

10 The steam generators sitting at about 1100
11 or 1200 psi perhaps the safety valves are open.
12 Saturation temperature at that pressure is about here.

13 This is the pressurizer volume, the
14 pressurize fills here. And we see that the cycle to
15 safety valves, we have four openings. And doing the
16 review I questioned the PORVs. Certainly the licensee
17 said, well we don't need the PORVs. We're not going
18 to take credit for the PORVs. We're qualifying the
19 safety valves for water relief. So we'll use the
20 safety valves to mitigate this event as we see here.
21 Safety valves are opening and closing. And they
22 qualify for water relief, so we can expect them to
23 close as designed.

24 However, the PORVs are going to be there.
25 And the PORVs will open first unless you have them

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1 blocked. I don't think that would be very likely. But
2 the PORVs once opened, you have to be sure that they
3 will close.

4 To qualify PORVs for water relief it takes
5 two steps: (1) the valves themselves have to be
6 qualified for water relief along with the discharge
7 piping, and; (2) the automatic control circuitry for
8 the PORVs has to be safety graded. And normally
9 that's not safety graded. And that's there to
10 guarantee that the PORVs will open when required and
11 will close when required.

12 In this case since the PORVs are not being
13 credited for mitigation of the event, we need to worry
14 only about the closing. In other words, if the
15 pressurizer fills and pressurized by the charging
16 pumps, it's possible that the PORVs will open. If they
17 open, we need to know that they'll close. If they
18 don't open, then we know that we have the safety
19 valves available. And this is what the transient here
20 shows; that the safety valves will handle this event.

21 So in response the applicant pointed out
22 the protection grade signal on low pressurizer
23 pressure that will automatically close the PORVs if
24 they should open.

25 MEMBER SIEBER: On the other hand if the

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1 PORV is not tested and qualified to pass water, even
2 though you get a close signal, it may not close,
3 right?

4 MR. MIRANDA: Yes. The EPRI valve tests
5 were used to qualify the PORVs for water --

6 MEMBER SIEBER: So they will close?

7 MR. MIRANDA: They will close if they get
8 a signal.

9 MEMBER SIEBER: Okay.

10 MR. MIRANDA: This is the mass flow rate
11 for the safety valves on the four openings.

12 MEMBER WALLIS: They will close if they
13 get a signal? Don't they sometimes stick?

14 MR. MIRANDA: Well, for the purpose of the
15 analysis if the valve is qualified under these
16 conditions, if PORV is not only used for steam
17 release; if it's qualified for water relief, we will
18 assume that it operates as designed. Because the
19 valve is qualified for water relief. And it is safety
20 graded, by the way. The PORVs themselves, the
21 components are safety grade. The problem is that the
22 circuitry is not safety graded. There are a couple of
23 single point failure vulnerabilities in the circuitry
24 that need to be corrected. That's for the opening
25 circuitry.

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1 For the closing circuitry that signal
2 comes from the protection system. So there will be a
3 reliable close signal.

4 MEMBER WALLIS: I thought TMI had a signal
5 that didn't close for mechanical reason. TMI had
6 boron deposits or something that stopped that closing.
7 Hey, you have plenty of signal.

8 MEMBER MAYNARD: Okay. But for this
9 accident you could have the same situation if a
10 qualified safety relief valve sticks open. Hence, you
11 go into your small break LOCA analysis. For this
12 analysis you're assuming that the valve closes there.
13 It for any reason it did not, you're still covered by
14 your small break LOCA analysis.

15 CHAIRMAN DENNING: And if you have a
16 monitor that says it didn't close, then you can close
17 a block valve the PORV?

18 MR. MIRANDA: Yes. Those are practical
19 considerations which are not relevant here.

20 CHAIRMAN DENNING: In regulatory space
21 you're saying?

22 MR. MIRANDA: Right. Because here they're
23 concerned about meeting that ANS criteria that says
24 you can't go to a condition III event. So if it
25 sticks open and if you're doing things like closing

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1 the block valve, you're mitigating a condition III
2 event. You've already violated the criteria.

3 This is also important here. This
4 pressurizer water temperature. The EPRI valve tests
5 showed that safety valves and PORVs, but safety valves
6 can be expected to function as designed if the water
7 temperature does not get too cold. For Crosby safety
8 valves which are installed in Beaver Valley Unit 2,
9 the temperature must not go below about 613 degrees.

10 MEMBER SIEBER: Put them in a box and put
11 a heater in there.

12 MR. MIRANDA: Excuse me?

13 MEMBER SIEBER: Put them in a box and put
14 a heater in there, which is what they did.

15 MR. MIRANDA: And for Beaver Valley Unit
16 1, which has Target Rock safety valves, they're much
17 better off with the water temperature for those valves
18 has to be above 330 degrees.

19 So these two plots are fairly important.
20 Eventually if you continue this, you will get below
21 613 degrees. But we can expect operator action to
22 occur before then. And this is the way the event is
23 mitigated. There's no automatic protection system
24 function such as reactor trip or other function that
25 will mitigate this event. It takes operator action.

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1 An operator must shut down the charging pumps. And
2 once that's done, the event is basically over. And
3 that will occur before the temperature reaches 613
4 degrees.

5 Westinghouse plants, there's a class of
6 Westinghouse plants in which Beaver Valley is included
7 but Ginna is not which use the charging pumps in the
8 safety injection system. And therefore, are
9 susceptible to this kind of a situation. And there
10 are ways to show that ANSI criteria is met.

11 One is to show that the operator acts
12 before the pressurizer fills to shut off the charging
13 flow. Another is to qualify the PORVs and to relieve
14 water by qualifying the PORVs themselves and the
15 discharge piping, and correcting the automatic control
16 system's circuitry. And six plants have done that;
17 Diablo Canyon, Callaway, Millstone have done that and
18 Salem also.

19 And the other option which Beaver Valley
20 has taken is to qualify the safety valves along with
21 taking credit for the closing signal coming from the
22 protection system.

23 So those are the three transients. Any
24 questions on those?

25 CHAIRMAN DENNING: Large LOCA lines, too?

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1 I didn't see it in the handout.

2 MR. MIRANDA: No.

3 CHAIRMAN DENNING: No? So you don't have
4 any large LOCA --

5 MR. MIRANDA: No, I don't.

6 CHAIRMAN DENNING: So basically for this
7 part you're done then?

8 MR. MIRANDA: I'm done, unless you have
9 any questions or you wish to talk about
10 overtemperature delta T or anything else. Do you want
11 to see transients like this for Ginna on Thursday.

12 CHAIRMAN DENNING: Yes.

13 MR. MIRANDA: Okay.

14 CHAIRMAN DENNING: Okay. We're done? Yes.
15 Okay. Thank you.

16 MEMBER WALLIS: Let's go back to modern
17 technology now. Note how sharp the last slides were.
18 You could even read the small print on those.

19 MR. FREDERICK: Again, I'm Ken Frederick.
20 I'm here to talk about the balance of the safety
21 analysis for Beaver Valley.

22 The last four subject areas we're going to
23 talk about small break LOCA, close LOCA long term
24 cooling and boron precipitation as well as
25 containment, containment conversion program primarily,

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1 containment overpressure credit and we'll briefly
2 touch on the dose assessment results.

3 To start off with small break LOCA. As
4 mentioned earlier, we're using NOTRUMP, which is the
5 current licensing basis for Beaver Valley and
6 Westinghouse approved methodology.

7 We have made some modifications to the
8 plant in order to retain or regain some of the margin
9 that we're losing for the EPU. The primary change
10 here is the higher head or higher capacity, high head
11 safety injection pumps. The increased flow associated
12 with that modification is around 5 percent.

13 We're also replacing some instrumentation
14 that gives us lower uncertainties which are factored
15 into how we set up the system, throttling.

16 We also increased the minimum SI
17 accumulator pressure and that provides some benefit
18 for the small break LOCA analysis.

19 During the course of the Staff review for
20 the small break analysis several questions were raised
21 for us to address. The first one dealt with the
22 methodology which Westinghouse was using concerning
23 the break spectrum.

24 Typical practice having to analyze
25 integer break sizes, for example 2", 3", 4". And the

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1 Staff felt that that was too course to capture the
2 maximum PCT.

3 Another issue which was raised was loop
4 seal clearing assumptions. The approved methodology
5 allowed for loop seal clearing on the broken loop but
6 not the intact loops. And our EPU analysis we had
7 other opinions of that methodology. Had actually
8 credited loop seal clearing on the intact loops as
9 well. So the Staff asked us to address that.

10 Another request from the staff was that
11 oxidation results for local oxidation needed to
12 include pre-transient oxidation. That's the oxidation
13 which occurs over the normal life of the fuel.

14 Another issue which was raised here was
15 for some of the smaller small breaks in the analysis
16 these things tend to hang up in terms of the PCT. And
17 primarily that's -- in fact, we reached kind of a
18 stagnation point.

19 The operators normally have a response
20 within a fairly small time frame. And we see the
21 slides of the PCT curves, we'll maybe talk about this
22 some more. Basically the concern here was that the
23 operator actions needed to be done in a timely manner
24 so that we could demonstrate refill of the core.

25 DR. BANERJEE: There's lots of little

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1 slides that we are missing.

2 MR. FREDERICK: Pardon me?

3 DR. BANERJEE: The previous one you had
4 those --

5 MEMBER SIEBER: He wants to see in that
6 little box.

7 DR. BANERJEE: Then give us an option.

8 MR. FREDERICK: This is basically a
9 pictorial explanation of loop seal clearing if you had
10 a question about what that is. Loop seals, of course,
11 are across under leg

12 CHAIRMAN DENNING: Go ahead. You can
13 proceed.

14 MR. FREDERICK: So we addressed the Staff
15 questions in this area. We did the analyses. We've
16 looked at break sizes down to quarter inch increments.
17 The allowance for loop seal clearing on the intact
18 loops within the analysis.

19 We also do -- normally this is always
20 done, but the burnup studies we did for oxidation and
21 that's looking at oxidation over the life of the fuel.
22 And we've included the pre-transient oxidation in that
23 calculation to show that we met with the pre-
24 transient.

25 This is the spectrum sizes that we've

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1 analyzed starting at 2 inch and going all the way up
2 to 6 inch. And in between 2 inches and 3 inches we
3 ran these smaller increments.

4 You can see there that the case of Unit
5 1 the peak clad temperature, the highest case ended up
6 being 2.75 inches where previously I think it was 3
7 inches. And for Unit 2 the worse case is still 3
8 inches. But, yes, there is a small -- something on
9 the order of for these analyses I think up to 60
10 degrees. For example 3 inches or 2 3/4 inches.

11 The other thing to note there as you get
12 into the smaller break sizes you can see that the
13 transients well out here past close to an hour. And
14 the theory there was that we need to take operator
15 actions, which is primarily to pull down,
16 depressurize, which allows the vessel to refill in
17 that time frame.

18 DR. BANERJEE: Do you get reflux
19 condensation in the steam generators for any of these
20 break sizes?

21 MR. FREDERICK: Josh from Westinghouse.

22 MR. HARTZ: Yes, this is Josh Hartz from
23 Westinghouse. I'm in charge of the neutron small break
24 LOCA evaluation model.

25 Yes, after the single and two phase

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1 natural circulation period when that mechanism breaks
2 down, the steam generators go into reflux cooling mode
3 and NOTRUMP does model that.

4 DR. BANERJEE: And all break sizes or some
5 break sizes and when does natural circulation stop and
6 when did you get into refluxing?

7 MR. HARTZ: Well, it's going to vary with
8 break size. If you get into larger break sizes, you
9 depressurize so quickly that you lose two phase
10 natural circulation so quickly that the break becomes
11 the dominant means of energy removal. So the reflux
12 condensation aspects tends to increase as break size
13 increases.

14 DR. BANERJEE: So at 2 inch, say, you'd
15 get refluxing but at 6 inch you wouldn't?

16 MR. HARTZ: More so than you would in the
17 6 inch break, that's correct.

18 DR. BANERJEE: Okay. Now you're going to
19 get more steam flow to the steam generator because
20 your power is greater by 10 percent, roughly, here?

21 MR. HARTZ: That's correct. Your boil off.

22 DR. BANERJEE: Now refluxing is effected
23 by flooding at the steam generator tube sheet inlet,
24 right? So can your steam generator inlet flow is
25 roughly the same because it's the same flow area that

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1 you have. Does the 10 percent increase in steam flow
2 lead to more water hold up in the steam generators or
3 not?

4 MR. HARTZ: NOTRUMP does show some liquid
5 hold up in the steam generators, but it doesn't tend
6 to dominate the results too much because we only see
7 it in the smaller breaks. But the --

8 DR. BANERJEE: Do you get any core level
9 depression due to that?

10 MR. HARTZ: Due to liquid holdup in the
11 steam generator we have seen it, but that tends to
12 make the results more conservative because the
13 differential pressure is driven up and it tends to
14 drive mixture level down. And sometimes make the
15 break flow stay at a low quality two phase mixture for
16 a longer period of time.

17 DR. BANERJEE: When you do these reflux
18 calculations, do you get flooding at the inlet of the
19 steam generators due to the steam flow or are you away
20 from flooding? Flooding defined as Graham Wallis
21 would.

22 MEMBER WALLIS: CCFL.

23 DR. BANERJEE: CCFL.

24 MR. HARTZ: The mechanism that we've seen
25 for these, and in some cases we have seen some

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1 flooding, but again it was for smaller breaks and that
2 mechanism tends to break down rather quickly. And so
3 it doesn't tend to have much dominance on the
4 transient.

5 DR. BANERJEE: Well, I'd be interested to
6 see the difference in this due to the increased steam
7 flow rates as to whether you get a more extended
8 period of flooding or not compared to pre-EPU as
9 opposed to post-EPU conditions. Because you're
10 getting 10 percent more flow rate, right? Now whether
11 this is giving you a larger period of flooding or not
12 is interesting for me to know.

13 So you take the 2 inch break, it doesn't
14 really matter.

15 MR. HARTZ: Okay.

16 DR. BANERJEE: Okay. Because you say
17 flooding breaks down quickly. It would only break
18 down if the core level went down somewhat so your
19 steam generation rate went down or because you're
20 getting the same stuff out of the break anyway,
21 right, in rough terms?

22 MR. HARTZ: That's correct, yes.

23 DR. BANERJEE: At these conditions. So
24 whatever goes to the steam generator is coming from
25 the core. So you're getting 10 percent more the core.

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1 So you would expect you'd get a more extended period
2 of flooding and more liquid hold up in the steam
3 generators and a larger core level depression. So I'd
4 like to see how -- just if we do this by hand, you can
5 more or less work it out using Graham's flooding
6 criteria CCFL to see whether this is in correspondence
7 with what you would expect by a hand calculation or
8 not.

9 MR. HARTZ: Well, one thing I might add is
10 there were some air water tests done with the steam
11 generator inlet plenum that were performed very early
12 on in NOTRUMP's development. And the model would be
13 based on that data. And what we could do is take a
14 look and see how the EPU would impact that.

15 DR. BANERJEE: Right. But there was
16 periods of this that occurred in Semiscale as well, if
17 I remember. So presumably NOTRUMP has been sort of
18 validated against those data as well?

19 MR. HARTZ: Yes, we used Semiscale as part
20 of our validation package.

21 DR. BANERJEE: So you've got some high
22 pressure validation data, too, right?

23 MR. HARTZ: That's correct.

24 DR. BANERJEE: Hopefully. So anyway, it's
25 worth finding out. Because one of the key aspects of

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1 this higher steam generation rate is the potential for
2 more liquid hold up. I'm not saying it would happen
3 here. It depends on the flow area of the steam
4 generator, all these things, obviously. So we take a
5 look at this aspect.

6 Thanks.

7 MR. HARTZ: Okay.

8 DR. BANERJEE: How many tubes are plugged,
9 you know, all this.

10 MR. HARTZ: Well, we assume different
11 plugging levels for each unit because Unit 1 has the
12 newer generators. Obviously, there would be less tube
13 plugging involved.

14 I believe Unit 1 assumed 10 percent and
15 Unit 2 22 percent.

16 DR. BANERJEE: Okay.

17 MR. FREDERICK: Let's go to the next
18 backup slide.

19 This is a plot which shows the transient
20 oxidation which is calculated over the burn up life of
21 the fuel, the red line. The green line is a
22 representation of a pre-transient type oxidation.
23 Normally that would go to zero at zero burn up.
24 However, this is cut off here at conservatively at
25 about 4 percent.

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1 And blue line is the addition of those
2 two.

3 So we show that over the life of the fuel,
4 17 percent criteria including pretransient oxidation.

5 MEMBER WALLIS: There's that much
6 pretransient oxidation? Yes, there is.

7 MR. FREDERICK: Yes. Essentially that
8 number corresponds to a fuel design limit. Now,
9 typically the actual does not approach that limit and
10 it's probably 50 to 75 percent of that. But it does
11 represent an upper bound that we use in the fuel
12 design.

13 Next slide, please.

14 This shows the results for the EPU
15 analysis as well as the current small break LOCA
16 analysis. You see here all the acceptance criteria
17 are met plus some 2200 for PCT and the hydrogen are
18 below the respective limits.

19 And this analysis reflects the
20 modifications we made to increase SI flow as well as
21 the accumulator pressure. So those changes tend to
22 offset the effects of EPU.

23 MR. HARTZ: Dr. Wallis, in case you're
24 wondering, those maximum hydrogen generation rates, we
25 just look at the hot assembly average. And if it's

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1 less than 1 percent, that's what we declare. But in
2 reality, as you know, not all the assemblies operate
3 at that power. So if you were to do an actual rod
4 census, it would be something much less than that.

5 MR. FREDERICK: No more questions on small
6 break. We're move on to post-LOCA long term cooling.
7 And this is the analysis that we do to demonstrate
8 that we do not reach precipitation limits for boron in
9 the core following a LOCA. And another criteria for
10 this analysis is that we show that we have enough flow
11 to meet the boron off and the flushing requirements.

12 CHAIRMAN DENNING: And what did you have
13 as the backup on this one. Because I'm definitely
14 interested in some particular. What's your backup
15 say?

16 MR. FREDERICK: This backup just shows the
17 alignment, the system type alignment for hot leg
18 recirculation.

19 CHAIRMAN DENNING: Okay. We may come back
20 to it. So go forward.

21 DR. BANERJEE: So you switched to hot leg?

22 MR. FREDERICK: On Unit 1 we switched to
23 a simultaneous hot and cold leg injection.

24 Again, as part of the NRC review we had
25 some questions in this area. Some of these were

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1 associate with I think some issues that came up from
2 Waterford. There were issues that we were asked to
3 address for this particular analysis, the first one
4 being core voiding must be part of the calculation for
5 the boron build up. There's some effects such as low
6 pressure drops are needed to be included.

7 If we were using a boric acid solubility
8 limit higher than base do pure water and boron or
9 elevated temperatures, then we needed to justify that.

10 And the Appendix K decay heat was the used
11 analysis.

12 So, again, in this case we redid the
13 calculations taking into consideration these issues.

14 CHAIRMAN DENNING: Now you're going to
15 have to help me because -- maybe it'll be clear on the
16 next. I'll wait before I ask some more questions.

17 MR. FREDERICK: So for the core voiding
18 aspect of this, we did more voiding calculations on a
19 transient basis using a modified Yeh Correlation.

20 CHAIRMAN DENNING: Now I don't understand
21 that. What does that mean, Yeh? You're using what
22 kind of analysis to determine what's happening within
23 the core and --

24 MEMBER WALLIS: Some sort of heat flux or
25 something or it's a -- isn't that the same thing.

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1 It's how you calculate the void fraction.

2 MR. FREDERICK: I'll ask --

3 MR. FINK: My name is David Fink. I work
4 for Westinghouse.

5 Dr. Wallis, that's correct it's kind of a
6 drift flux. It's a way just to calculate the voiding.

7 MEMBER WALLIS: I think it's actually
8 benchmarked against the rod bundles and things. Real
9 Geometry is like this, so --

10 MR. FINK: I believe it is.

11 CHAIRMAN DENNING: Okay. Now tell me
12 again. The vehicle that's doing the analysis, how is
13 it modeling the system?

14 MR. FREDERICK: It's a fairly simplistic
15 analysis. Essentially you're looking at the core and
16 then the boil off rate and the --

17 CHAIRMAN DENNING: So it's the equivalent
18 of a RELAP analysis where you would look in -- and why
19 not? I'm missing how you're going to determine -- I'm
20 concerned about the way volumes are mixed under the
21 assumption of when the boron concentrates and you get
22 increased density there, it's not clear to me that
23 you're adequately considering what's really happening
24 axially up the channel and whether as you get more and
25 more bubble formation within the channel, whether

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1 that's offsetting the increased density due to
2 concentration of boron. Can you give me a better idea
3 as to how you're actually analyzing the flow
4 characteristics of what's happening in the core.

5 MR. FREDERICK: Dave, do you want to take
6 that?

7 MR. FINK: Yes. This is David Fink again.

8 If I could take a minute here and just
9 explain. The original analysis that we did for the
10 Beaver Valley EPU actually in the time line was
11 several years ago. So they were actually pre-
12 Waterford uprate. Okay. Those analyses used a simple
13 control volume calculation and much as we've done for
14 25, 30 years for hot leg switch over calculations.

15 And in those simplified control volume,
16 you have a boiling pot, you have steam coming out, you
17 have borated water going in and you build up boric
18 acid in the core region. Okay.

19 So for the uprate the difference is more
20 power, more boil off, faster build up. Okay.

21 In that very simplified approach there
22 were two big conservatism at least as we believe it.
23 And the first was how we selected the control volume.
24 Okay. The control volume that's historically been
25 used didn't include any of the lower plenum. It didn't

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1 include any of the volume --

2 MEMBER WALLIS: Uniform mixing in this
3 whole control volume? Surely when you have boiling in
4 a channel the boron is sort of pumped along and then
5 as the steam evolves, the boron's left behind. So it
6 concentrates at the top, doesn't it?

7 MR. FINK: Well, our simplified model
8 assumed complete mixing in the core region.

9 MEMBER WALLIS: There's some experiments
10 that show that's reasonable?

11 MR. FINK: Well, we believe there's quite
12 a bit of circulation going on in the core region. For
13 example --

14 CHAIRMAN DENNING: Why do you believe
15 that? Why do you believe that? That's what I want to
16 know.

17 MR. FINK: Well, we've looked at our large
18 break LOCA WCOBRA/TRAC code and we've looked at what
19 happens in the core region in that code.

20 CHAIRMAN DENNING: Now, which specific
21 accident is the one of concern here?

22 MR. FINK: This is all large break.

23 CHAIRMAN DENNING: Large break?

24 MR. FINK: Yes, sir.

25 CHAIRMAN DENNING: Okay. So that you have

1 essentially atmospheric conditions at the outlet, is
2 that true?

3 MR. FINK: Yes, sir.

4 CHAIRMAN DENNING: Okay. And you have a
5 big level swell kind of situation in terms of the
6 voiding -- as you get near the upper part, there's a
7 bigger and bigger froth.

8 MR. FINK: Okay. Well, I can just
9 continue here.

10 CHAIRMAN DENNING: Yes.

11 MR. FINK: So that was what we originally
12 did for the first go around.

13 MEMBER WALLIS: Dry regions? If you have
14 dry regions presumably the boron's left behind on the
15 wall.

16 DR. BANERJEE: If there was core uncovering.

17 MEMBER WALLIS: Right. Or you had
18 spattering, a spattering of cooling and you have
19 spattering cooling rather than froth cooling, but the
20 boron's left behind on the wall.

21 CHAIRMAN DENNING: If you'd like to use
22 that board over there to illustration, you can also do
23 that. If that would help.

24 DR. BANERJEE: Back to that screen.

25 CHAIRMAN DENNING: But not the screen.

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1 MR. FINK: I might do that.

2 So in response to NRC RAIs, and this was
3 largely I guess posed Waterford fallout and specific
4 RAIs asked by the Staff for these calculations, we did
5 this work. Okay. And we addressed the four things
6 that are listed up on the board, most significantly
7 was the use of Appendix K decay heat, which these
8 calculations have always been based on a best estimate
9 decay heat. And so we used Appendix K decay heat. We
10 also calculated a time based core voiding. And all
11 that does is that reduces the liquid volume in your
12 control volume. Okay.

13 So we did those calculations. Because we
14 are now taking a lot of liquid volume out of the core
15 region we choose to credit some volumes that were not
16 previously credited, and probably the most significant
17 is the one that was discussed during the Waterford
18 EPU, which is the lower plenum.

19 MEMBER WALLIS: There's an experiment. I'm
20 trying to remember the name of it, isn't there?

21 MR. FINK: It was the MHI BACCHUS Test.

22 MEMBER WALLIS: BACCHUS. It was a god of
23 some sort. BACCHUS. This seemed to show that things
24 really were mixed?

25 MR. FINK: Yes. Yes, it did.

1 MEMBER WALLIS: Surprising to us.

2 MR. FINK: It clearly showed --

3 DR. BANERJEE: Yes, it is surprising. Can
4 you explain that test again.

5 MR. FINK: Well, the test clearly showed
6 the point at which the denser higher concentrated
7 region up in the core becomes dense enough to displace
8 the less concentrated volume in the lower plenum. So
9 in the test you could clearly see as the --

10 MEMBER WALLIS: Heavy concentrate --

11 DR. BANERJEE: I mean isn't there a
12 countervailing flow which is balancing that?

13 MR. FINK: Well, under this scenario this
14 is a cold leg break where all your excess SI flows out
15 the break. So more SI doesn't help you. You
16 basically have a stagnant boiling pot and you're
17 feeling through the lower plenum enough to make up boil
18 off, but --

19 DR. BANERJEE: And that's not enough for
20 the density head being developed? It allows you to
21 settle the borated water against that flow?

22 MR. FINK: Well, the flow that's coming in
23 is coming from the sump and it's coming --

24 MEMBER WALLIS: In the BACCHUS report?

25 DR. BANERJEE: Who did these experiments?

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1 MR. FINK: MHI.

2 DR. BANERJEE: Who is that?

3 MR. FINK: Mitsubishi Heavy Industries.

4 DR. BANERJEE: And these were done where
5 in --

6 MR. FINK: These were done in a scale
7 facility they did specifically to look at this.
8 Because Japanese plants to this day still use a 24
9 hour switchover time, which was the original
10 Westinghouse design.

11 MEMBER WALLIS: So it's a big facility, as
12 I recall. It was scale, but it was still fairly big?

13 MR. FINK: Yes. It was a slab model, so it
14 was like full length, 180th scale, I believe.

15 DR. BANERJEE: And so they had borated
16 water boiling off on heaters or something?

17 MR. FINK: Correct.

18 DR. BANERJEE: And they had a lower plenum
19 markup and they looked at the density profile?

20 MR. FINK: Well, they had it highly
21 instrumented with boron sensors and temperature
22 sensors. And we wrote a summary report that was
23 presented for the Waterford EPU. And I'm sure the NRC
24 has a copy of it. It's very interesting.

25 DR. BANERJEE: But do you have a copy of

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1 the BACCHUS report itself?

2 MR. FINK: It's a MHI test, so we wrote a
3 summary report that is part of --

4 MEMBER WALLIS: Right. I saw it. I think
5 it was in the Waterford context. We spent some time
6 on this.

7 MR. FINK: Yes.

8 DR. BANERJEE: So your contention is that
9 the whole thing is well mixed, not just the core.

10 MEMBER WALLIS: So what's your point? But
11 once you get enough density difference it turns over,
12 doesn't it?

13 MR. FINK: That's correct. And we'd like
14 to credit the whole lower plenum to give us a little
15 better answer, but we conservatively credited as was
16 done for Waterford. We just credited 50 percent of the
17 lower plenum as being a reasonably conservative
18 approach.

19 DR. BANERJEE: What happens if you don't
20 credit it?

21 MR. FINK: Well, it's just how much liquid
22 volume you have in your calculations. So you have --

23 DR. BANERJEE: Right. So suppose you just
24 stayed with your old assumption of allowing mixing in
25 the core region and nowhere else?

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1 MR. FINK: Well, then the boric acid would
2 build up faster.

3 MEMBER WALLIS: I guess we had a lot of
4 questions previously about whether just looking at
5 solubility limits was good enough when you're boiling
6 off this -- when it gets concentrated the boron,
7 presumably, can precipitate around nucleation sites
8 and things like that. It's not as if just solubility
9 alone is governing whether or not you get some
10 precipitation. And if you have some drop wise
11 cooling, then if a drop evaporates it leaves behind
12 its boron. So we had questions of that type. I don't
13 know if they were ever answered. Because you just
14 look at the overall solubility, don't you?

15 MR. FINK: That's correct.

16 MEMBER WALLIS: I think we asked the Staff
17 to look into this, didn't we, Ralph?

18 MR. CARUSO: Yes. And they presented.

19 MEMBER WALLIS: Yes, then we were
20 satisfied. We spent some time on it, I know.

21 DR. BANERJEE: So are we revisiting
22 something that was --

23 MEMBER WALLIS: Yes, we went into it. We
24 spent a whole day or something like this.

25 DR. BANERJEE: Done.

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1 MR. CARUSO: Yes.

2 MEMBER WALLIS: But you should get the
3 BACCHUS report.

4 DR. BANERJEE: All right.

5 MEMBER WALLIS: It's all about Roman
6 orgies and things like that.

7 DR. BANERJEE: It sounds like it.

8 MEMBER WALLIS: It's a good report. You
9 should get it. It could tell you some things that
10 wouldn't be intuitive if you just thought about it.

11 CHAIRMAN DENNING: I'd like some
12 information on the third bullet on --

13 MR. KELLERMAN: Yes. My name is Brett
14 Kellerman. I'm with Westinghouse. And we can get
15 access to a summary report of the BACCHUS test that we
16 brought for the Waterford --

17 MEMBER WALLIS: We probably have that in
18 the record somewhere. The Waterford record, we have
19 it. You can just pull it out and give it to him.

20 CHAIRMAN DENNING: But you do it, like in
21 the third bullet there, you do have some information
22 on sump additives as they effect boric acid
23 solubility, is that what I'm seeing there?

24 MR. FREDERICK: Yes. Similar to what
25 Waterford had at I believe their TSP plant.

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1 MR. FINK: Yes. This is Dave Fink again.

2 In these analyses we do not credit any
3 elevated solubility limit due to sump additives for
4 this uprate.

5 MEMBER WALLIS: Additives are presumably
6 chemicals?

7 MR. FINK: Yes.

8 MEMBER WALLIS: They're not fibers?

9 MR. FINK: I hope not.

10 DR. BANERJEE: There's also a possibility
11 that it wouldn't mix because there'll be enough fiber
12 at the core inlet, right?

13 MEMBER WALLIS: Well, that's another
14 question. Yes.

15 MR. FREDERICK: We did a test using sodium
16 hydroxide and we found that the precipitation limit
17 increased from 29 percent up to about 48 percent. But
18 we are not crediting that as part of our analyses.
19 And we did use decay heat.

20 MEMBER WALLIS: It should be part of the
21 sump question, though, when you get fines going
22 through the screens. Would that make any difference
23 to his picture?

24 MR. FREDERICK: Yes. That's something that
25 I believe is going to be addressed as part of the

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1 downstream --

2 MEMBER WALLIS: Under GSI-191.

3 MEMBER WALLIS: -- effects under GSI-191.

4 Yes.

5 DR. BANERJEE: Suppose that it didn't mix
6 outside the core region, for whatever reason, it could
7 be that the core inlet is blocked with debris --

8 CHAIRMAN DENNING: The problem may be
9 worse than that if that happens.

10 DR. BANERJEE: Well, there's some bypass
11 paths through the --

12 MEMBER WALLIS: The sump?

13 DR. BANERJEE: Yes. So then what happens
14 to the boron if it's boiling off happily in the core
15 without this assumption of mixing with the lower
16 plenum? Is it then an untenable --

17 MR. FINK: Yes. You'd have a
18 precipitation limit much sooner and --

19 DR. BANERJEE: Yes. Is it an untenable
20 situation then or is it still okay? Do you have to
21 make this assumption or do you not to make it
22 liveable?

23 MR. FREDERICK: Well, if we ended up with
24 a shorter time, say 3 hours or 4 hours or something,
25 not necessarily --

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1 DR. BANERJEE: Is that still okay?

2 MR. FREDERICK: --untenable but we would
3 have to look at what our makeup rates could be. So we
4 did a test here as we need enough flow to meet the
5 boil off and also flush the core.

6 DR. BANERJEE: Because if I remember the
7 report that was circulated by Ralph, you have 6 hours
8 to do the switchover, is that right?

9 MR. FREDERICK: That's correct.

10 DR. BANERJEE: Yes. So at the moment if
11 you didn't credit half the lower plenum, which is a
12 large volume, and only had the core, would this be
13 like 2 hours, 1 hour, 3 hours? What would be that
14 number?

15 MR. FREDERICK: Do you have a feel for
16 that, Dave?

17 DR. BANERJEE: Because the volume is very
18 different, right?

19 MEMBER SIEBER: Yes.

20 MR. FINK: This is Dave Fink.

21 The lower plenum's actually a pretty good
22 size volume, but because we're crediting half of it,
23 it probably represents maybe one-fourth -- maybe one-
24 third, one fourth of the total volume. So it would --

25 MEMBER WALLIS: So it would feed or

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1 something in total --

2 MR. FINK: Correct.

3 MEMBER WALLIS: And the core --

4 MR. FINK: So is representing a third of
5 the volume you'd increase.

6 DR. BANERJEE: Well, what is the core
7 volume that you're crediting?

8 MR. FINK: I believe with the one-half
9 lower plenum volume and the core voiding, we're
10 probably -- I'd say approximately 900 cubic feet.

11 DR. BANERJEE: And of that about 300 is
12 lower plenum?

13 MEMBER WALLIS: Half of it. Half of it.

14 DR. BANERJEE: Half of it.

15 MEMBER WALLIS: A 150.

16 MR. FINK: I'd say that's --

17 DR. BANERJEE: So the core volume is so
18 large.

19 MEMBER WALLIS: Don't get it all because
20 there are voids in it.

21 DR. BANERJEE: I see.

22 MR. FINK: Well, it's core and upper
23 plenum, so it's --

24 DR. BANERJEE: Well, why the upper plenum
25 if it's boiling off. Wouldn't that get full of steam

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1 or something?

2 MR. FINK: Well, we look at the way this
3 calculation is done, we do the voiding at the top of
4 the core at the core exit. And we apply that voiding
5 up through the upper plenum. So the upper plenum does
6 contribute.

7 DR. BANERJEE: But the upper plenum is not
8 empty in this case?

9 MR. FINK: That's correct.

10 DR. BANERJEE: So the steam is going out
11 through the hot leg, is that right?

12 MR. FINK: Correct.

13 DR. BANERJEE: Eventually it makes its way
14 out to the cold leg break somehow, around the circuit?

15 MR. FINK: Correct.

16 DR. BANERJEE: So why is the upper plenum
17 not full of steam?

18 MR. FINK: The upper plenum would be full
19 of some mixture, some voided --

20 MEMBER WALLIS: Otherwise you can't drive
21 the water along the hot leg, presumably.

22 DR. BANERJEE: There's no water going on--

23 MEMBER WALLIS: Right. You dry out --

24 DR. BANERJEE: It's mainly steam, right?
25 It's mainly steam going along?

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1 MEMBER WALLIS: Yes, but --

2 DR. BANERJEE: Maybe a sketch would help
3 because I'm sort of a bit lost as to where all the
4 water is in this system. So can you just sketch it?

5 MR. FINK: Ken, do we have a backup slide
6 that might have that?

7 DR. BANERJEE: I mean the simple control
8 volume approach is great, but we got to put the water
9 in the right places here.

10 MR. FINK: Well, we don't credit anything
11 outside of the vessel, outside of the inside of the
12 core barrel actually in this calculation. So we don't
13 credit any of the volume in the former region or the
14 downcomer.

15 MEMBER SIEBER: Or that?

16 MR. FINK: No, no.

17 MEMBER SIEBER: That's a significant
18 amount of water.

19 MR. FINK: Yes, sir.

20 DR. BANERJEE: Yes. Show us what you're
21 crediting --

22 MEMBER WALLIS: Here are the levels down
23 below the hot leg.

24 DR. BANERJEE: That's what I thought it
25 would be, but for some reason you have a volume of

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1 mixing above.

2 MR. FINK: Well, in that picture
3 everything we're crediting is right inside that inside
4 cylinder that represents the core. So we don't
5 crediting anything outside of that.

6 MEMBER WALLIS: Credit the downcomer at
7 all?

8 MR. FINK: Correct.

9 DR. BANERJEE: Okay. So how much is that
10 volume that you would credit if you didn't credit any
11 piece of the lower plenum here?

12 MR. FINK: Up to the bottom of the hot
13 leg, I believe it would be 1,000 cubic feet.

14 MEMBER WALLIS: With the bubbles or not?

15 MR. FINK: That would be total volume.

16 DR. BANERJEE: Only the core?

17 MR. FINK: Correct.

18 DR. BANERJEE: Okay. And then if you
19 credited 50 percent of the lower plenum, it's another
20 300.

21 MEMBER WALLIS: One fifty.

22 MR. FINK: Approximately.

23 DR. BANERJEE: One fifty. Okay. So it's
24 not such a big deal.

25 MR. FINK: It's actually a little more

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1 than 150, I believe.

2 DR. BANERJEE: All right. I think that's
3 fine. If that -- that sounds good.

4 MEMBER WALLIS: Well, I think the thing is
5 when you're so close to the limit, you've got to darn
6 sure that it's well mixed. Because all you need is to
7 have a little bit of nonmixing and you have twice as
8 much concentration in the top as in the bottom and you
9 get precipitation. So you really have to study the
10 BACCHUS report to be convinced that there's good
11 mixing.

12 MR. FINK: There are some other
13 conservatism in the methodology. For example, we don't
14 credit any entrainment around the loops that might
15 take place early on where you'd expect to carry a lot
16 of water around the loops. So we start our problem
17 from the beginning. And that probably represents a
18 great deal of conservatism.

19 We've always had trouble identifying
20 exactly how much entrainment you'd get around the
21 loops.

22 CHAIRMAN DENNING: Do you know offhand
23 what the void fraction is in the upper plenum that
24 you're talking about? What's the void fraction?

25 MR. FINK: Probably I'm guessing 70

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1 percent.

2 CHAIRMAN DENNING: Seventy percent?

3 MR. FINK: Seven percent.

4 CHAIRMAN DENNING: Even though there's
5 that much void fraction, the density of that material
6 is higher than the density of the material than the
7 cold water in the lower plenum?

8 MR. FINK: It would be the density of the
9 liquid, and you'd have to as you went down into the
10 core and into the periphery is where you'd be much
11 less voiding.

12 MR. FREDERICK: This slide actually shows
13 the collapsed liquid load that was calculated.

14 DR. BANERJEE: Where's the bottom of the
15 core?

16 MR. FINK: The 12 foot level there is the
17 top of the core. So that's collapsed liquid level.

18 DR. BANERJEE: Right. But where is the
19 bottom of the core?

20 MR. FINK: Zero.

21 DR. BANERJEE: Zero? All right.

22 MEMBER WALLIS: At some previous time this
23 was dried out on top?

24 DR. BANERJEE: At zero -- time zero.

25 CHAIRMAN DENNING: Right. This is much

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1 later. Sometime it was dried out.

2 DR. BANERJEE: Early times.

3 MEMBER WALLIS: And when it was dried out
4 didn't you get boron precipitation on the dried out
5 part?

6 DR. BANERJEE: That was the large break
7 LOCA.

8 MEMBER WALLIS: Yes, but you get it in the
9 small break, too, otherwise you never get these high
10 temperatures. Well, they get boron plating on these
11 tubes. But anyway Staff convinced us that we're not
12 to worry about it I think before.

13 MR. FREDERICK: Go back one slide.

14 MEMBER WALLIS: Move on probably.

15 CHAIRMAN DENNING: Yes. Right. Let's move
16 on. I think some of us are going to want to look at
17 that BACCHUS report again today.

18 MEMBER WALLIS: Because it's a very
19 interesting subject.

20 MR. FREDERICK: In the draft SER there was
21 an item identified as a contingency for this
22 particular analysis. And it has some discussions with
23 the Staff about that issue. It's described here, and
24 basically the concern was that for smaller breaks we
25 need to demonstrate the capability that we'll be able

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1 to cool down before the precipitation time in order to
2 be able to -- the actual injection on the hot legs.
3 An we've had some discussions with the Staff on that
4 issue. And Dr. Ward will be talking about that later.
5 At this point we're convinced we have a --

6 CHAIRMAN DENNING: I guess I'm a little
7 bit confused about the difference between large LOCA
8 case and then the small LOCA cases that you were
9 talking about as far as what the conditions are that
10 could lead to precipitation and can you help me there?

11 MR. FREDERICK: Well, I think for small
12 breaks typically and your temperature and your
13 pressure is going to hang up. So precipitation limits
14 are very high under those conditions. The concern
15 would be that borrowing that scenario who hold on the
16 pressurization mode, want to make sure that you get to
17 the cooled down condition before you reach
18 precipitation limit for the cold condition. That,
19 again, is a function of the operator response to the
20 event.

21 DR. BANERJEE: Because if you inject in
22 the hot leg, you get cold water into the core, right?
23 Is that the concern?

24 MR. FREDERICK: That's not the major
25 concern. The major concern is depressurizing enough so

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1 we get hot leg flow. Because for Unit 1, anyway, we're
2 aligning the low head pumps to the hot legs and it
3 would have a shot off pressure of around --

4 MEMBER WALLIS: Once you get hot leg flow,
5 you just flush the boron out.

6 DR. BANERJEE: Yes.

7 MR. FREDERICK: Again, Dr. Ward will be
8 discussing --

9 MEMBER WALLIS: Now you need to keep
10 enough boron in to avoid criticality concern? And
11 you've already scrambled the reactor --

12 DR. BANERJEE: Well, the water's is
13 borated, isn't it?

14 MEMBER WALLIS: Yes. Don't you need still
15 boron for the criticality.

16 DR. BANERJEE: In the injection --

17 MEMBER SIEBER: The injection water is
18 refueling water.

19 MR. FREDERICK: So again, we have
20 addressed the questions that were raised by the Staff
21 for this analysis and the results showed for Unit 1 6½
22 hours is the required switchover time, 6 hours for
23 Unit 2.

24 In our procedures we actually make
25 preparations to do that realignment an hour ahead of

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1 time. The actually alignment is only a matter --

2 MEMBER WALLIS: This time depend on the
3 break size?

4 MEMBER SIEBER: It should.

5 MR. FREDERICK: Essentially no, because at
6 the point where we're starting the calculations you're
7 fixed in terms of the volume of water in the --

8 DR. BANERJEE: Well, in long term cooling,
9 which is within an hour --

10 MEMBER WALLIS: -- off to atmospheric
11 without any break size contributing.

12 MR. FREDERICK: Yes, heat boil off at that
13 point.

14 MEMBER WALLIS: At the point of water
15 boiling, essentially an open top.

16 CHAIRMAN DENNING: But it's still
17 pressurized.

18 MR. FREDERICK: Large break, it's not in
19 the small break.

20 CHAIRMAN DENNING: Right. But in the
21 small break it is.

22 MEMBER WALLIS: Well then how much is
23 pressurized must depend on the break size?

24 CHAIRMAN DENNING: Yes.

25 MEMBER WALLIS: And so the time surely

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1 depends on the break size, doesn't it?

2 MR. FREDERICK: David?

3 MR. FINK: This is David Fink again.

4 The effect of some pressure assumption in
5 the vessel really helps you in the voiding. So at
6 higher pressures you get a lot of this voiding --

7 MEMBER WALLIS: You have more water there.

8 MR. FINK: A lot more water.

9 MEMBER WALLIS: So there's nothing magic
10 about 5 hours, is there? I mean sometimes it depends
11 on the break size. So what it is the operator
12 measures so that he knows he has to do something?

13 MR. FREDERICK: From the start of the
14 event.

15 MEMBER WALLIS: But he doesn't know the
16 break size, so he doesn't really know --

17 MR. FREDERICK: Yes. The time that we're
18 calculating it represents the bounding case.

19 CHAIRMAN DENNING: The bounding case?

20 DR. BANERJEE: Doesn't he have some
21 indicator to know when it would be prudent to
22 switchover? Like isn't there a measurement of some
23 sort that --

24 MR. DURKOSH: I'm going to try to answer
25 that. This is Don Durkosh from FirstEnergy.

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1 The emergency operating procedures are
2 based on the limiting large break LOCA switchover
3 time. We do not have any other measurements. We
4 basically will follow our EOP network and we'll be in
5 our E1 procedure waiting for this switchover time to
6 occur, and then we'll be preparing for it. And we'll
7 initiate switchover. So there is no other
8 measurements. In theory, we don't know where the
9 break size is so we set it up for the most limiting
10 conditions there.

11 MEMBER WALLIS: If it were smaller, he
12 would have longer time?

13 DR. BANERJEE: So there are no criteria
14 which requires switchover?

15 MR. FREDERICK: They're all the type
16 criteria --

17 DR. BANERJEE: No, no, no. Physical
18 criteria.

19 MEMBER WALLIS: There's not a measurement
20 that you compare with some other measurement --

21 DR. BANERJEE: Now I'd better switch
22 because things are getting bad or something.

23 MEMBER WALLIS: No. He's just told within
24 so many hours to do it.

25 MR. FREDERICK: There's no way to measure

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1 the boron --

2 MEMBER WALLIS: He has to remember?

3 DR. BANERJEE: Really of the neutron flux,
4 right, in the core? You still have some sort of a flux
5 measurement, right, something?

6 MR. FREDERICK: Yes. I guess if the
7 source range was operational still, yes, we would have
8 some indication. I'm not sure how you would correlate
9 that to boron levels, though.

10 DR. BANERJEE: So you don't have a measure
11 of boron? So you have no measure of boron in the core
12 basically?

13 MR. FREDERICK: Dave, did you have
14 something?

15 MR. FINK: This is Dave Fink.

16 Actually, they don't do it but you could
17 in theory measure the boron by the boron concentration
18 in the sump because all the boron that you're leaving
19 behind in the vessel is coming from somewhere. And
20 that somewhere is the sump. So as the vessel
21 concentration's building up, the sump is diluting. So
22 theoretically you could --

23 DR. BANERJEE: But is the sump so large in
24 volume that dilution would be relatively small
25 compared to the --

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1 MEMBER SIEBER: It would not look the same
2 as the core condition from a chemistry standpoint.
3 Concentrating mechanisms in the core, the sump has
4 everything else.

5 DR. BANERJEE: Right.

6 MEMBER SIEBER: And so the concentrations
7 would be different.

8 DR. BANERJEE: Would be not -- yes.

9 MEMBER SIEBER: Does -- help you at all in
10 knowing where you're at?

11 MEMBER WALLIS: At levels lower in the
12 core?

13 MEMBER SIEBER: Yes.

14 MR. DURKOSH: This is Don Durkosh again.

15 MEMBER WALLIS: EOPs don't speak to that.

16 MR. DURKOSH: Yes. The switchover time is
17 institutionalized in the EOPs. They're consistent for
18 all Westinghouse plants. And this is the approach
19 that we've been using since literally day one. We use
20 these times as the time to go ahead and initiate
21 switchover to hot leg recirc.

22 DR. BANERJEE: It could be too early, it
23 could be too late; we don't know. There's no way to
24 know.

25 MEMBER SIEBER: Well, it's based on the

1 analyses.

2 DR. BANERJEE: On calculations, right?
3 Who knows what these calculations mean, how good they
4 are.

5 MEMBER WALLIS: But it's been done since
6 day one.

7 MEMBER SIEBER: The calculations were done
8 by the Westinghouse owners group at the time that the
9 guidelines were done.

10 DR. BANERJEE: Therefore they must be
11 good?

12 CHAIRMAN DENNING: So this is how it's
13 changed by the EPU?

14 MEMBER SIEBER: That was back in 1981 or
15 '82.

16 MR. FREDERICK: If you consider the
17 calculations bounding and very conservative, as this
18 slide shows you here, we actually ran cases with more
19 realistic assumptions. And you can see trying to get
20 to the limit, which is 29 percent here. Well, you
21 can't actually see it. But considerable difference
22 when you consider better estimate type assumptions.
23 And, Dave, maybe you can --

24 MEMBER WALLIS: More significant perhaps
25 is the effect of EPU on this?

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1 MR. FREDERICK: No, this is just --

2 MEMBER WALLIS: No. More significant
3 would be to show the effect of EPU?

4 MR. FREDERICK: Well, the EPU ended up
5 reducing the time from 8 hours to 6½.

6 MEMBER WALLIS: Yes.

7 MEMBER SIEBER: And that's basically due
8 to the increased decay heat.

9 MEMBER WALLIS: Yes. But you assume
10 that's not critical? I mean, it's still got an awful
11 long time.

12 MR. FREDERICK: Yes. Again, it's not
13 challenging the operators to get it done. So the more
14 meaty concern with shortening that time is that the
15 higher you go up on the decay heat curve, the more
16 flow you need. And --

17 MEMBER WALLIS: There's some sort of alarm
18 clock that starts when there's a break and then after
19 6 hours says you'd better switchover injection or is
20 he supposed to keep track of all the time?

21 MEMBER SIEBER: You have blogs.

22 CHAIRMAN DENNING: That's a good EOP
23 question, I think.

24 MR. FREDERICK: Yes.

25 MR. DURKOSH: This is Don Durkosh again.

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1 The operating crew would keep track of
2 what time the reactor trip and we'd have the technical
3 support center available to us, we have our STAs
4 available to us. So we have multiple people basically
5 keeping track. And we have an explicit step in our E1
6 emergency procedure. We would transition back into our
7 E1 procedure and we'd basically, the next step would
8 be when you approach the hot leg switchover time,
9 begin making your preparations.

10 So we have various people that would tab
11 of that time.

12 MEMBER WALLIS: It still would be good if
13 you had something that alerted him. I mean, if I have
14 to cook something, I don't really look at my watch all
15 the time. I like to have a timer that tells me when
16 to switch things off or take them out of the oven.
17 But this is an EOP question.

18 I think the more you can take away from
19 the operator having to remember things, the better.
20 You have something which actually tells him he's got
21 to do something.

22 But anyway, it's not really --

23 CHAIRMAN DENNING: I think we're ready to
24 move out of that into containment analysis.

25 MEMBER WALLIS: Yes, I think -- yes.

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1 MR. DURKOSH: This is Don Durkosh.

2 We do have timers in the control room

3 MEMBER WALLIS: You do?

4 MR. DURKOSH: But unlike cooking, we do
5 also have a lot of people available to us.

6 MEMBER WALLIS: Too cooks --

7 MR. FREDERICK: Too many cooks in the
8 kitchen.

9 MEMBER SIEBER: You have to remember to
10 turn the timers over.

11 CHAIRMAN DENNING: Go ahead and continue.

12 MR. FREDERICK: Okay. I'm going to move
13 on to containment analysis. Again, the containment
14 analysis was submitted actually a little earlier than
15 EPU in June of 2004, and that was approved in February
16 of this year.

17 And it was a conversion, which mean we
18 went from a sub-atmospheric design to an atmospheric.
19 The difference there being that in the atmospheric
20 design there's no requirement to contain or to get
21 back to sub-atmospheric conditions post accident,
22 which we had previous to the change.

23 The primary effect of EPU, which was
24 factored into this containment conversion program, was
25 the M&Es from the primary system and the steamline

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1 break. Those are really the things that are directly
2 affected by the increase in power.

3 The mass and energy release calculations
4 for this program use the Westinghouse approved
5 methodologies, and that wasn't a change.

6 For the containment integrity, part of the
7 calculations, we utilized MAAP-DBA, which is a
8 modification to MAAP 4 which changed some of the
9 containment calculations.

10 It's similar to the other codes which have
11 been used or approved for applications such as GOTHIC,
12 COCO.

13 The program the containment uses
14 traditional heat transfer correlations such as Tagami
15 and Uchida. That's consistent with other
16 applications.

17 For the NPSH calculations we've
18 incorporated a multi node model. And that allows us to
19 get better details on where water is held up in
20 containment and certain volumes. At the box area you
21 can just see the nodal model that we used. Eighteen
22 nodes.

23 For small break analyses, and we've done
24 a much more extensive look at small break primarily
25 for sump inventory questions. For that analyses the

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1 mass and energy releases were calculated using MAAP.
2 And those results were benchmarked against the code
3 primarily.

4 The actual operating containment pressure
5 will still be slightly sub-atmospheric at the site
6 14.3 approximately is atmospheric pressure. And our
7 operating range will be 12.8 to 14.2 absolute.

8 The older operating pressure, which is
9 actually an air partial pressure limit, was about 4
10 pounds lower. So at these higher pressures we
11 eliminate the need for applied air when we do make
12 entries, which is a very nice benefits in terms of
13 personnel safety.

14 MEMBER SIEBER: Well, and you have
15 decompression in the airlock, which is a time consumer
16 and hard on some people, hard on your ears.

17 MR. FREDERICK: As part of this analysis
18 we've also credited the various modifications which
19 are beneficial. Replacement steam generators for Unit
20 1, for example. These generators have the restriction
21 nozzle in the outlet where our old ones did not. So
22 we're looking at 4.6 square foot main steamline break
23 versus a 1.4 square feet. So that is a big benefit
24 for the steamline break analysis.

25 Also the feed isolation and the cavitating

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1 venturies, again, limit the mass energy release during
2 a steamline break.

3 MEMBER MAYNARD: Are those new valves or
4 just new actuators or --

5 MR. FREDERICK: They're brand new valves
6 and actuators.

7 MEMBER MAYNARD: Okay. Are they replacing
8 existing valves that are there or --

9 MR. FREDERICK: There was an existing
10 valve there. I believe we turned that into a check
11 valve, is that right?

12 MR. TESTA: Yes. This is Mike Testa,
13 Beaver Valley.

14 Yes, like Ken was saying, we had a check
15 valve in the system that had a motor on it. And what
16 we ended up doing was we restored that to just a
17 normal or simple check valve. And then in the piping
18 system we added a brand new feed isolation valve. New
19 valve, new actuator controls.

20 MEMBER SIEBER: It is hydraulic or
21 electric or --

22 MR. TESTA: Hydraulic. Yes.

23 MR. FREDERICK: We've also added a cord
24 from the reactor cavity so there's the general
25 basement area that allows the water that normally hold

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1 up in that cavity to drain back into the sump, which
2 helps out with our inventory issues.

3 This QS cutback was a feature that we used
4 to extend the spray at Unit 1 that helped us maintain
5 some of the spurious condition. We don't need that
6 any longer so we're eliminating it.

7 And again, the setpoint for transfer to
8 recirc was lowered under this program and that gives
9 us a little higher sump level at recirc, which helps
10 out with the NPSH.

11 For the analysis, essentially acceptance
12 criteria that we look at:

13 Peak pressure, of course, less than the
14 design, which is 45.

15 Containment pressure reduction of 50
16 percent, that's essentially an assumption that's made
17 in the offsite dose analysis so we need to demonstrate
18 that we can meet that;

19 NPSH. We need the required NPSH for the
20 pumps which takes suction out of the sump, and;

21 When the pumps start we look at minimum
22 pump inventory to make sure we don't have any
23 vortexing issues.

24 MEMBER WALLIS: Of course, that's all
25 assuming that the screens don't have too much

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1 deposited on them?

2 MR. FREDERICK: Correct.

3 MEMBER WALLIS: What kind of insulation do
4 you have on this?

5 MR. FREDERICK: Insulation?

6 MEMBER WALLIS: Yes. Kind of insulation?
7 Do you have fiberglass or --

8 CHAIRMAN DENNING: That's the physics.

9 MEMBER WALLIS: But I wasn't here. I
10 wasn't here. I'm sorry.

11 CHAIRMAN DENNING: If you could give a
12 little summary.

13 MEMBER SIEBER: It's reflective.

14 MR. FREDERICK: But I know and then Mark
15 can maybe jump in. We do have RMI reflective on many
16 of the components. We do have CALSIL.

17 MEMBER WALLIS: You have CALSIL?

18 MR. FREDERICK: Yes. We have CALSIL and we
19 have something Min-K, which I -- it's a fiber.

20 MR. MANOLERAS: This is Mark Manoleras.

21 We have very small quantities of that
22 material. We're going to target that for removal, that
23 material for removal.

24 DR. BANERJEE: That's the only fibrous
25 material? Is that the only fibrous material?

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1 MR. MANOLERAS: That would be our
2 predominant fibrous material.

3 DR. BANERJEE: And do you have aluminum as
4 well?

5 MR. MANOLERAS: Yes, we do. Yes, we do.
6 And we actually have a program which takes a look and
7 monitors and maintains the quantities of aluminum in
8 containment. We know exactly what we have. Zinc and
9 aluminum in containment.

10 MEMBER WALLIS: You have TSP in the sump?

11 MR. MANOLERAS: No, we do not.

12 MR. FREDERICK: Carbon hydroxide.

13 MEMBER WALLIS: Carbon hydroxide.

14 MR. MANOLERAS: Correct.

15 DR. BANERJEE: Carbon hydroxide and
16 aluminum is --

17 MEMBER WALLIS: Yes.

18 CHAIRMAN DENNING: You can continue.
19 Thanks.

20 MEMBER WALLIS: Yes.

21 DR. ELAWAR: This table shows the peak
22 pressure results for the LOCA and steamline breaks as
23 well as the pre-EPU results.

24 You see here, for example, Unit 1
25 steamline break, that pressure actually went down even

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1 though we're analyzing for EPU conditions. And, again,
2 that's reflecting the beneficial modifications that
3 were made there.

4 And essentially all these results benefit
5 to some degree from the methodology change to MAAP-
6 DBA. Again, we're raising initial pressure 4 pounds
7 for these, so obviously we're getting some margin.

8 CHAIRMAN DENNING: When you show the pre-
9 EPU, is that post-containment conversion?

10 MR. FREDERICK: No.

11 CHAIRMAN DENNING: No, that's pre-
12 containment--

13 MR. FREDERICK: Prior.

14 MEMBER WALLIS: That's using a previous
15 method of calculation?

16 MR. FREDERICK: Yes. It's using the Stone
17 & Webster program.

18 MEMBER WALLIS: Okay.

19 DR. BANERJEE: What is the difference in
20 the methods of calculations which give you the slide
21 again?

22 MR. FREDERICK: Hit the backup slide.

23 This slide shows essentially how the peak
24 pressure is sensitive to airborne water fractions. And
25 that water fraction is essentially the water coming

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1 out of the break, what percentage of it is actually
2 entrained into the atmosphere. In the previous
3 methodology essentially there was no entrainment
4 assumptions. It looked at other programs such GOTHIC.
5 GOTHIC actually assumed a 100 percent entrainment.

6 MEMBER WALLIS: Oh.

7 MR. FREDERICK: And when we looked at
8 this, the curve basically once you get to 10 percent,
9 you don't get much more benefit. But 10 percent --

10 MEMBER WALLIS: There's a fog in there,
11 you're saying there's a fog in there?

12 MR. FREDERICK: Yes. The water at
13 entrainment essentially acts like an additional heat,
14 so it gives you a benefit in the peak pressure.

15 MEMBER WALLIS: Airborne water fraction is
16 the faction of the water which is entrained?

17 MR. FREDERICK: Yes.

18 DR. BANERJEE: Emitted?

19 MR. FREDERICK: The fraction of the water
20 that is coming out of the break that is entrained.

21 MEMBER WALLIS: I would think getting a
22 100 percent of it would be a bit of a struggle,
23 getting it all help up in the air. It's going to fall
24 out, isn't it?

25 MR. FREDERICK: Well, some of it is, yes.

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1 DR. BANERJEE: I think, I mean most of it.

2 MEMBER WALLIS: Most of it.

3 MR. FREDERICK: Well, we did provide as
4 part of the submittal, we provided some comparisons to
5 experimental data. I don't remember the experiments
6 right off hand. But those results showed somewhere in
7 the 50 to 60 percent range were entrained.

8 DR. BANERJEE: But you have surfaces where
9 the water jet impacts, right?

10 MR. FREDERICK: Yes, and that does account
11 for that. If there is collisions with surfaces and
12 poor condensation for that matter, it is removed in
13 that--

14 DR. BANERJEE: But nonetheless, it's a
15 heat sink?

16 MR. FREDERICK: Yes, essentially.

17 MEMBER WALLIS: When you start out you've
18 got to make a lot of dispersion. But as you put more
19 and more water in there, there must be a lot of it
20 that comes out?

21 MEMBER KRESS: Why isn't that below 45?

22 MR. FREDERICK: It's absolute. But this is
23 not for our plant in particular. This is just --

24 MEMBER KRESS: Oh, I see. This is just for
25 some plant.

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1 MEMBER WALLIS: So what do you do? You
2 assume something here or what?

3 MR. FREDERICK: Actually, for MAAP we
4 assume 10 percent entrainment.

5 MEMBER WALLIS: It's just someone's
6 educated guess?

7 MR. FREDERICK: It was a conservative
8 relative to what we saw in the experiments.

9 MEMBER WALLIS: Well, it's interesting.
10 How much mass of water is it then when it's 10
11 percent? Later in a LOCA it's a lot, isn't it? The
12 air is holding all that up?

13 MEMBER SIEBER: You get a number of them.

14 CHAIRMAN DENNING: Well, wait a second.
15 This is the large break and early time peak.

16 MEMBER WALLIS: Time is --

17 MR. FREDERICK: Yes, this is all currently
18 in the first 20 seconds.

19 MEMBER WALLIS: So it's probably okay.
20 Early time, yes.

21 MR. FREDERICK: Yes.

22 MEMBER WALLIS: Everything's stirred up.

23 MR. FREDERICK: Yes, it's very quick. Yes.

24 MEMBER WALLIS: I was concerned when you
25 say you assume something.

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1 MR. FREDERICK: Just to cover the other
2 criteria and results, we did show that we met the
3 depressurization rate, time. NPSH requirements were
4 satisfied. We also look at EQ, for example, if the
5 envelopes change, we look at the equipment and we've
6 done that. And as well as the structural issues, the
7 piping and the sump inventory.

8 The next subject which is related --

9 MEMBER SIEBER: Before you leave, you said
10 that even with the relaxation of the sub-atmospheric
11 requirement you still returned to some sub-atmospheric
12 condition following a LOCA. How long does that take?
13 An hour?

14 MR. FREDERICK: I'm not sure I said that,
15 Jack. But we can still get there is the river is cold
16 enough. I mean, this is very much a function of the
17 service water temperature.

18 MEMBER SIEBER: Okay.

19 MR. FREDERICK: Typically though --

20 MEMBER SIEBER: You don't necessarily go
21 sub-atmospheric.

22 MR. FREDERICK: That's right. Right.

23 MEMBER SIEBER: And so from a Part 100
24 standpoint if you have some positive pressure --

25 MR. FREDERICK: And if some leakage

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1 occurs--

2 MEMBER SIEBER: -- you may see it on the
3 outside, right?

4 MR. FREDERICK: For the dose analyses we
5 assume leakage occurs for 30 days.

6 MEMBER SIEBER: Okay.

7 MEMBER KRESS: I think the section there
8 is you use that high for the peak pressure after 24
9 hours, right?

10 MR. FREDERICK: That's reduced to half of
11 that within 24 hours.

12 MEMBER KRESS: Regardless of what it
13 really is? I mean, it's usually lower than that.

14 MR. FREDERICK: Yes.

15 MEMBER KRESS: But it's a conservative
16 calculation?

17 MR. FREDERICK: Oh, yes.

18 Moving on to containment overpressure.
19 For Beaver Valley Unit 1 the recirc spray pumps have
20 credited in the past containment overpressure as part
21 of our existing licensing basis. And for this analysis
22 containment conversion and EPU we're continuing to
23 credit that.

24 Unit 2 does not require any containment
25 overpressure --

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1 MEMBER WALLIS: Are you crediting the same
2 amount of overpressure for the same amount of time?

3 MR. FREDERICK: I'll touch on that. We
4 have some slides that show that.

5 Unit 2 does not credit overpressure and
6 never has. Physically the pumps are a lot lower so
7 they don't have a need for that.

8 The Beaver Valley recirc spray system,
9 essentially this is our heat removal function post-
10 LOCA in the environment that each train consists of a
11 pump, heat exchanger and spray ring. And it takes
12 suction directly from the sump and delivers a spray
13 flow for Unit 1.

14 MEMBER WALLIS: When you need it is when
15 you have the high pressure in the containment.

16 MR. FREDERICK: That's correct, yet. The
17 system was primarily designed to give you a rapid
18 depressurization so you could meet the one hour sub-
19 atmospheric requirement.

20 The backup slide just shows a sketch of
21 the system, basically.

22 MEMBER WALLIS: Does it show the pressure
23 needs versus time or something like that and how much
24 you're actually crediting?

25 MEMBER KRESS: They're different.

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1 MR. FREDERICK: Yes.

2 MEMBER WALLIS: That's coming up?

3 MR. FREDERICK: About 2 slides.

4 MEMBER WALLIS: We're waiting for that.
5 That's the bottom line.

6 MR. FREDERICK: We're there. This slide
7 shows you the containment over pressure required.

8 MEMBER WALLIS: You need 10 psi.

9 MR. FREDERICK: The COP required is
10 basically how much pressure do I need above the
11 initial pressure in containment to get enough NPSH.
12 So, yes, when the pumps first start out, and again
13 these pumps start relatively early, 5 minutes after we
14 reach the high pressure setpoint in containment. So
15 the sump is relatively hot at that point and there is
16 not a lot of level. So the NPSH is somewhat limited.
17 So we need containment overpressure at that point.

18 Well, let me make another point here. This
19 shows the previous results from pre-EPU and actually
20 pre-containment conversion.

21 MEMBER WALLIS: The Staff didn't give you
22 any trouble with the blue lines so then they're going
23 to accept the red line?

24 MR. FREDERICK: Yes. The blue line is
25 occurring, as you can see, for the EPU we're

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1 increasing--

2 MEMBER WALLIS: And you already have? You
3 already have that approved the blue line?

4 MR. FREDERICK: That's correct, yes. The
5 increase in actual pressure requirement is on the
6 order of 2 pounds. Duration wise this requirement goes
7 below zero, which means that we don't really need
8 overpressure at that point.

9 MEMBER WALLIS: Not a very long a period
10 of time compared with some plants.

11 MR. FREDERICK: That's correct, yes. The
12 point here is that it's roughly ten minutes past the
13 start of the pump.

14 MEMBER WALLIS: And for hours?

15 MR. FREDERICK: Right.

16 MEMBER SIEBER: For the inside research
17 spray pump.

18 MR. FREDERICK: Correct. And this is for
19 the outside.

20 MEMBER SIEBER: Right.

21 MR. FREDERICK: It's very similar.

22 MR. MANOLERAS: This is Mark Manoleras
23 again.

24 Ken, why don't you go into detail on the
25 testing of the pumps.

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1 MR. FREDERICK: Yes, I'll get to it. It's
2 a couple of slides away yet.

3 MEMBER WALLIS: Run without this COP?

4 MR. FREDERICK: Next one.

5 This slide shows the available
6 overpressure against the required, the two bottom
7 lines being the required. And what you can see here
8 is actually when the pumps start. They actually start
9 delivering flow about 300 seconds.

10 MEMBER WALLIS: Now this pressure that's
11 available looks very high. Usually people make a lot
12 of conservative assumptions. This looks like the real
13 pressure. You're going up to 40 psi.

14 MEMBER SIEBER: Yes.

15 MEMBER KRESS: This is atmospheric.

16 MR. FREDERICK: This is actually
17 overpressure.

18 MEMBER WALLIS: Yes.

19 MEMBER SIEBER: Containment pressure.

20 DR. BANERJEE: You have a pretty small
21 containment, right, to get that?

22 MEMBER SIEBER: Smaller than --

23 MEMBER WALLIS: Usually you have a
24 containment pressure that's high like that which you
25 use to evaluate the integrity of the containment.

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1 MR. FREDERICK: Right.

2 MEMBER WALLIS: And then you have a sort
3 of minimum curve which has all kinds of conservative
4 assumptions, which is much lower. And I don't see
5 that there.

6 MR. FREDERICK: Well, again, you may not
7 see it so much in the peak because that's not really
8 effected by what we do in terms of trying to minimize
9 the pressure.

10 MEMBER WALLIS: It's not?

11 MR. FREDERICK: You know, it's when you
12 start the sprays and the peak is basically a function
13 of how Tagami ends up. It's based on volume, energy
14 release and the timing. So that's not something that
15 would really change much.

16 MEMBER WALLIS: So is this blue curve
17 conservatively estimated to be below the real
18 pressure?

19 MR. FREDERICK: Yes. We do sensitivity
20 studies that look at really the whole event, not just
21 pressure because it's also a function of sump
22 temperature. And some things that tend to reduce
23 pressure also reduce sump temperature. So both of
24 those are in the NPSH equation. So what we have done
25 historically is we do sensitivity studies on all the

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1 sensitive parameters and determine what is the minimum
2 NPSH available case, which is what's shown here.

3 MEMBER WALLIS: Well, this really should
4 say minimum available overpressure or something, not
5 a best estimate kind of calculation.

6 MR. FREDERICK: No. This is actually the--

7 MEMBER WALLIS: The conservative minimum.

8 MR. FREDERICK: This case reflects the
9 minimum NPSH available result.

10 DR. BANERJEE: No. I mean the blue curve
11 is the minimum containment pressure available? I mean
12 if it's just about --

13 MR. FREDERICK: It may not necessarily be
14 the minimum available. It's the minimum available
15 associated with the set of conditions that come to
16 this analysis.

17 DR. BANERJEE: With this -- yes. Sure.
18 But for this set of conditions it's a large break LOCA
19 or something, right?

20 MR. FREDERICK: Yes.

21 MEMBER KRESS: We once wrote a letter that
22 said those calculations ought to have probabilities in
23 them to see how much the probabilities overlap to get
24 some sort of probability that you would have --

25 DR. BANERJEE: No. Uncertainty anyway.

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1 MR. FREDERICK: And we actually have some
2 stuff in here on that, too.

3 MEMBER KRESS: Yes.

4 DR. BANERJEE: If not probability, at
5 least uncertainty.

6 MEMBER KRESS: Uncertainty. Yes.

7 MEMBER WALLIS: We did write the letter.
8 We got several members who endorsed additional
9 comments, wasn't that --

10 MEMBER KRESS: Yes, as I recall.

11 CHAIRMAN DENNING: You only spray in
12 recirculation mode? You don't spray from the
13 refueling water start --

14 MR. FREDERICK: No, we do both.

15 CHAIRMAN DENNING: You do both?

16 MR. FREDERICK: Yes, and that's what you
17 can see here. I mean, we're going from 40 pounds down
18 to nothing in a little over 10 minutes.

19 CHAIRMAN DENNING: That's due to spray?

20 MR. FREDERICK: Yes. So once the spray
21 start, we have a quench spray system which comes from
22 the RST which is --

23 MEMBER WALLIS: If the pumps weren't
24 working, the blue code would be higher? So it's a
25 kind of self-controlling situation?

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1 MR. FREDERICK: That's correct, yes. The
2 reason we need overpressure is because we're running
3 the sprays. And you can see the pressure comes down
4 pretty quickly once those sprays go on.

5 MEMBER WALLIS: The sprays themselves
6 reduce the overpressure?

7 MR. FREDERICK: That's correct.

8 MEMBER SIEBER: And if you didn't have the
9 overpressure, you wouldn't need the sprays.

10 MR. FREDERICK: The problem with not
11 having the sprays is that it's our only means of
12 getting heat out of the sump.

13 MEMBER SIEBER: Right.

14 MR. FREDERICK: We need the heat
15 exchangers more than we need the sprays.

16 MEMBER SIEBER: Right.

17 MEMBER WALLIS: When you need the sprays,
18 they work?

19 MR. FREDERICK: Yes.

20 DR. BANERJEE: Those little side diagrams,
21 maybe we should get copies of those because they have
22 -- yes.

23 MR. FREDERICK: Just a point there. Again,
24 that was the NPSH limited case. It's not necessarily
25 the longest duration. For all the cases we look at,

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1 the most amount of time that we need for overpressure
2 credit is 20 minutes after the pump starts.

3 And we did do some testing of these pumps
4 way back in the late '70s. Actually, it was North
5 Anna pump that was tested, but they're basically
6 identical to ours.

7 Hit this backup slide. They actually ran
8 these pumps at reduced NPSH all the way down to about
9 4 feet available, the left line there. And basically
10 you can see, as you reduce NPSH below the required,
11 the performance suffers. But they ran these up to
12 about a half hour in this reduced NPSH mode.

13 MEMBER SIEBER: And they still pump?

14 MR. FREDERICK: And they still pumped and
15 they tore them down, and there was no damage to the
16 pumps.

17 DR. BANERJEE: Well, there was some
18 cavitation, but --

19 MR. FREDERICK: Yes, obviously it's
20 offering in a cavitation --

21 DR. BANERJEE: Not significant. Not until
22 to --

23 MEMBER WALLIS: Until they fall off the
24 cliff there.

25 MEMBER KRESS: Even with the required net

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1 positive suction you had some cavitation, right?

2 MR. FREDERICK: Yes, 3 you're percent
3 reduced by definition.

4 MEMBER KRESS: Yes. Yes.

5 MR. FREDERICK: Go back.

6 DR. BANERJEE: Excuse me. Go back to that
7 slide.

8 What is there, I can't read that very
9 well, but what is the suction head required. Yes, I
10 can't read the ones on top there.

11 MR. FREDERICK: (Off microphone).

12 MEMBER SIEBER: You have to talk into a
13 microphone.

14 MR. FREDERICK: Right.

15 DR. BANERJEE: Is that 16, 14? The four
16 I can read, but beyond 4 I can't read any of those.
17 They're blurred.

18 MEMBER WALLIS: Are you saying that even
19 if there were no overpressure available they'd still
20 work? If you lacked 10 psi, will they still work or
21 not?

22 DR. BANERJEE: These are in feet of water,
23 I take it.

24 MEMBER WALLIS: Twenty feet of water, do
25 they still work at 20 feet of water.

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1 DR. BANERJEE: No, there are 4 feet of
2 water, they would work.

3 MEMBER WALLIS: Yes, but not at 20?

4 DR. BANERJEE: No, at 20 they'd work
5 perfectly.

6 MEMBER WALLIS: Oh. Well, you've got 4
7 feet, don't you? What is that you need? You need--

8 DR. BANERJEE: 11.5 feet. Is that your
9 reference is, 11.5 feet of NPSH on this?

10 MR. FREDERICK: For these pumps the
11 minimum required that we use is 9.8 feet.

12 DR. BANERJEE: 9.8 feet. All right. So
13 that's the one, Graham, which is the fourth line down
14 from the top.

15 MEMBER WALLIS: That one there?

16 DR. BANERJEE: That's your reference,
17 right?

18 MR. FREDERICK: Yes.

19 MEMBER WALLIS: And how compact can it get
20 and still satisfy your needs there?

21 MR. FREDERICK: Four feet available, that
22 would be something around 2 psi overpressure --

23 MEMBER WALLIS: It's still pumping.

24 MR. FREDERICK: -- still required.

25 MEMBER WALLIS: But that's much less than

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1 you're asking for?

2 MR. FREDERICK: Yes. This is a kind of
3 margin we don't use these lower limits in anyway or we
4 don't model the pumps in a degraded performance.

5 MEMBER WALLIS: It seems to depend a lot
6 on the dynamic head required. How much is the dynamic
7 head required? There's a load line somewhere here.

8 DR. BANERJEE: Right, that's what I was
9 going to ask. Where is that load line? Just
10 conceptually if you sketch it.

11 MR. FREDERICK: Well, these pumps normally
12 operate around 33 to 3500 so your system curve comes
13 through here somewhere.

14 MEMBER WALLIS: So some of those have
15 already crashed and gone over the -- they went over
16 the precipice by the time they come down to the load
17 line?

18 MR. FREDERICK: Well, yes, you would see
19 a much reduced flow but you would still get some flow.

20 CHAIRMAN DENNING: But in reality isn't it
21 just a matter that you don't want them to fail.
22 Because suppose for 20 minutes they didn't work and
23 they didn't remove heat, isn't this really a real long
24 term problem that you're concerned about, which is
25 long term heat removal.

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1 MR. FREDERICK: Yes.

2 CHAIRMAN DENNING: So the fact that
3 they're not able to keep up with heat rejection during
4 this period when you really need it doesn't really
5 matter.

6 MR. FREDERICK: If we have reduced heat
7 removal, the ultimate effect is that the sump's a
8 little hotter a little longer.

9 MEMBER WALLIS: So you'll get 2000 GPM
10 instead of 3500 or something?

11 MR. FREDERICK: Right.

12 MEMBER WALLIS: And it's no big deal?

13 CHAIRMAN DENNING: As long as you --

14 MR. FREDERICK: It only last for 10 or 20
15 minutes, yes.

16 MEMBER MAYNARD: I think the more
17 significant part of this what shows is that they
18 operated for a long period of time, it reduced NPSH
19 and did not fail the pumps and they were still in good
20 shape.

21 MR. FREDERICK: Yes.

22 CHAIRMAN DENNING: Okay. Continue.

23 MR. FREDERICK: Next.

24 We looked from the PRA aspect of this, you
25 know what's the probability of losing containment

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1 isolation which could lead to loss of overpressure.
2 And we estimated that to be about one times 10 to the
3 minus 8. And that's based on the LOCA coincident with
4 failure of isolation for the lines that communicate
5 directly with the containment atmosphere. And those
6 lines for Beaver Valley are actually pretty small. The
7 largest such line is a 2 inch line.

8 CHAIRMAN DENNING: Since you're still
9 operating a little bit sub-atmospheric, does that help
10 your probability here? Do you know that you're
11 isolated?

12 MR. FREDERICK: Yes. Essentially we would
13 screen out any large preexisting failure because we
14 would notice that if it occurred.

15 DR. BANERJEE: Is there any interaction
16 with a LOCA which would sort of tend to make you lose
17 containment isolation?

18 MR. FREDERICK: No. All of our
19 containment --

20 DR. BANERJEE: Nothing that --

21 MR. FREDERICK: -- systems are fully
22 qualified.

23 DR. BANERJEE: Completely independent?

24 MR. FREDERICK: Yes. We actually did an
25 analysis where we looked at -- you know, essentially

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1 run the NPSH cases with holes in containment. And we
2 did up to a 3 inch based on what our penetration size
3 are.

4 And if you look at the next slide here
5 essentially all the results are on top each other so
6 there is no significant effect of opening a small hole
7 in containment. Again, that was the most probable
8 based on the actual penetration sizes that are open to
9 containment atmosphere.

10 DR. BANERJEE: But then what happened to
11 the pressure as you open the hole?

12 MR. FREDERICK: It didn't change much.

13 CHAIRMAN DENNING: You can't tell at that
14 small hole size.

15 MR. FREDERICK: Right. Essentially
16 there's a minimal change in the pressure response such
17 that the NPSH margin doesn't change much.

18 Next slide.

19 We do a conservative analysis in terms of
20 minimizing the overpressure available. We do not ask
21 the operators to intervene in anyway to try and
22 maintain pressure at a certain value or certain limit
23 to try and assure that we have available COP.

24 MEMBER WALLIS: Suppose the screens were
25 getting block, how would the operator know it and what

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1 would he do?

2 MR. FREDERICK: I'll let my operator
3 handle that one here.

4 MR. DURKOSH: This is Don Durkosh again.

5 Recently, probably within the last year or
6 so, we've implemented sump blockage guidelines. And
7 we've updated our emergency procedures. So basically
8 when we enter the recirc mode we have RNO, response
9 not obtain actions where we would start a pump or
10 verify a pump is running. And we would monitor things
11 like pump amps, discharge pressure and flow. And if
12 we see any variations, then we have a sump blockage
13 guidelines available to us.

14 And in the big scheme what the sump
15 blockage guidelines really do is have you look for
16 ways to reduce flow, which would reduce the line
17 losses across the sump screens. So basically kind of
18 get you to reduce the flows, get NPSH back into an
19 acceptable range and operate in that mode.

20 MEMBER WALLIS: You don't backflush or
21 anything like that?

22 MR. DURKOSH: Not at this time.

23 MEMBER MAYNARD: I wouldn't think that the
24 things you would be looking for would be much
25 different than what you in mid-loop operation, making

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1 sure that your RA pumps are cavitating or lose
2 suction. I mean it would be a similar situation with
3 the sump.

4 MR. DURKOSH: I agree.

5 MEMBER MAYNARD: Yes.

6 DR. BANERJEE: Are we going to talk about
7 sump blockage at some point?

8 MEMBER WALLIS: Yes, you are.

9 CHAIRMAN DENNING: You already have as
10 much as we are.

11 DR. BANERJEE: Because it was be
12 interesting to know how difficult it would be to
13 backflush.

14 MEMBER WALLIS: I think it's taboo,
15 though.

16 CHAIRMAN DENNING: Yes, I think we
17 shouldn't be talking about that now, no.

18 MEMBER WALLIS: That's another subject.

19 CHAIRMAN DENNING: I mean it's interesting
20 to see what they are going to do.

21 DR. BANERJEE: But you're going in for an
22 EPU. You may as well put it in.

23 MEMBER WALLIS: Yes, but it's a generic
24 issue.

25 MR. CARUSO: Yes, but it's a generic issue

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1 and we don't resolve generic issues.

2 DR. BANERJEE: Okay. We won't resolve it.

3 MEMBER WALLIS: You don't dump it all on
4 one licensee.

5 CHAIRMAN DENNING: We just initiate
6 generic issues under this.

7 Okay. Proceed.

8 MR. FREDERICK: Just to finish up this
9 slide, we did look at potential modification that
10 could be made to eliminate the need for containment
11 over pressure and essentially they're all impractical.

12 MEMBER WALLIS: I'm curious. You're
13 putting in a bigger screen. What design is it?

14 MR. FREDERICK: Design in terms of -- hit
15 the back slide.

16 MEMBER WALLIS: This is a whole lot of
17 cylinders or --

18 MR. FREDERICK: Yes, it's an array of
19 cylinders.

20 MEMBER WALLIS: An array of cylinders.

21 DR. BANERJEE: But is this the top hat
22 design.

23 MR. FREDERICK: Yes.

24 MEMBER WALLIS: Okay. Ah, so the problem
25 there is to figure out how that performs when you've

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1 only tested one?

2 DR. BANERJEE: Yes, it's the same problem-

3 MR. FREDERICK: Our testing is actually
4 looking at it.

5 MEMBER WALLIS: Testing arrays?

6 MR. FREDERICK: I think we're do a 9 set
7 of array.

8 MEMBER WALLIS: Oh, okay. Okay. Thank
9 you. That's better than one.

10 MEMBER SIEBER: It looks like that would
11 take up a lot of space.

12 DR. BANERJEE: Then it would be prudent to
13 do backflushing.

14 MEMBER WALLIS: It's not difficult to
15 figure out that works.

16 MR. FREDERICK: Just summarizing I guess
17 for the containment overpressure, COP is required for
18 Beaver Valley Unit 1 RS pumps. And it's part of the
19 licensing basis. And it's continued to be credited in
20 the recently approved submittal.

21 We have run these pumps at reduced NPSH
22 with satisfactory results. And we looked at the risk
23 of losing overpressure, and it's very low. And we
24 also looked at modifications to eliminate the need,
25 and they're not practical.

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1 The next two slides --

2 CHAIRMAN DENNING: You can go quickly on
3 these I think.

4 MR. FREDERICK: Yes. These essentially
5 summarize the dose assessment results from the
6 accident analyses.

7 Again, we're moving to full implementation
8 of the alternative source term and we've updated X/Qs
9 with more recent meteorological data and we've also
10 switched to ARCON 96 for the onsite X/Qs.

11 We've incorporated the results from our
12 control room tracer gas testing.

13 Unit 2 continues to use the alternate
14 repair criteria, which develops the accident induced
15 leakage limits. And all the results are within the
16 50.67 limits, as you can see on the next slide.

17 Again, here the Unit 2 value is maximized
18 based on the alternate repair criteria methodology.

19 Just to summarize for safety analysis.
20 Again, we've looked at the required events. All the
21 acceptance criteria seem to be met at the EPU
22 conditions. And we feel like we have enhanced the
23 plant in some way with the modifications we've made
24 and are beneficial impacts in terms of the safety
25 margin. And we've been able to retain a lot of the

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1 safety margin.

2 That's it. Any questions?

3 CHAIRMAN DENNING: Are there any questions
4 on safety analysis here? Anything that we want to
5 prod for more information tomorrow?

6 MEMBER WALLIS: I want to know what the
7 Staff thinks about the containment overpressure, but
8 that's not any of that today.

9 CHAIRMAN DENNING: That's to come.

10 Okay. Thank you very much.

11 We're now going to go in recess until by
12 that clock up there it's going to be -- we'll make it
13 a quarter of by that clock.

14 (Whereupon, at 3:33 p.m. a recess until
15 3:50 p.m.)

16 CHAIRMAN DENNING: Okay. We're now back in
17 session. And we're now going to hear about the
18 Staff's view of safety analysis SBLOCA.

19 DR. WARD: Can you hear me? Okay.

20 My name is Len Ward, I'm in NRR in the
21 code review analysis branch. And what I'm going to
22 talk about, I'm going to talk basically about post-
23 LOCA long term cooling, and that's large and small
24 break, but then I'm also going to talk about short
25 term behavior small break LOCA.

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1 But before I do that, what I wanted to do
2 is just quickly go over the ECCS system that's used to
3 control boric acid, what's the approach. And then I'll
4 talk about large break LOCA and small breaks.

5 Now Beaver Valley, it's a 3 loop plant.
6 It's about an 8 percent power increase.

7 MEMBER SIEBER: Do you want a pointer?

8 MR. LEE: Yes, you know, I thought I had
9 one here. Here we go.

10 A key ingredient here in this plant is
11 that it has three accumulators. And as you heard
12 earlier, the pressure was increased to 625 pounds and
13 that's key for short term small break LOCA behavior.

14 And I'll also be talking about the switch
15 to simultaneous injection and because of the way the
16 ECCS is aligned, because of the ECCS configuration,
17 cold let breaks are limiting in this plant for boron
18 precipitation.

19 As I said, large breaks to control boric
20 acid, you realign the ECCS, that's the high pressure
21 safety injection pump to deliver half the flow in the
22 hot leg and the other half in the cold leg. And I'll
23 be showing you some calculations that I did to audit
24 the precipitation times that the licensee performed.

25 I'm also going to talk about small breaks.

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1 And it was mentioned before, but small breaks you can
2 hang up at a higher pressure. You don't go down to 147
3 where you're basically at run out on that high
4 pressure pump. You had some intermediate pressure.
5 It could be 200 pounds, 100 pounds. When you split
6 the flow between both legs it's not enough the flush
7 the core. So what do you do? Well, you cool the
8 plant down. And you cool the plant down to a low
9 enough pressure so that you either get it low enough
10 so that you can flush the core when you switch
11 simultaneous injection or you've cooled it down low
12 enough and fast enough so that you refill the RCS with
13 ECCS coolant, you reestablish single phase natural
14 circulation and you disperse the boron. Okay? And
15 I'll show you some calculations that we did to
16 illustrate that.

17 MEMBER WALLIS: Even though there's a
18 break, you can fill that whole thing?

19 DR. WARD: That's right. We're talking
20 small breaks, one inch, two inch, three inch; they're
21 really tiny. You'll fill it back up. I'll show you
22 that when I get to the slide.

23 MEMBER SIEBER: It's the pot. The break's
24 above the pot.

25 DR. WARD: The break's in the cold leg.

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1 MEMBER SIEBER: Right.

2 DR. WARD: Or the hot leg. And the
3 alignment is done such that you don't need to know
4 where the break is. And the analysis is done so you
5 don't need to know necessarily. It's nice to know what
6 the concentration in the core and vessel is, but you
7 don't need to know that. If you do a bounding
8 calculation on precipitation time, all the operators
9 have to know is when the accident started and at
10 certain times you just go switch. And it doesn't
11 matter what the break location is or where the break
12 is.

13 DR. BANERJEE: When the HPSI are there
14 line sizes indicator of the flows or is it --

15 DR. WARD: No, that's just where it's
16 going.

17 MEMBER WALLIS: It's not to scale or
18 anything?

19 DR. WARD: This is not to scale. So what
20 I want to do is to show you for a cold leg break,
21 before you switch to simultaneous injection you're
22 injecting into the downcomer. You're storing some of
23 it out the break.

24 MEMBER WALLIS: Right.

25 DR. WARD: But because there's no flush,

1 okay, you're going to concentrate boric acid in the
2 vessel, in the upper plenum in the core. And
3 basically -- let me use this. This is better.

4 I mean what happens is you're going to
5 fill the downcomer to the bottom of the cold leg. You
6 can't get anymore water in there because the break's
7 there. Any more water you add spills.

8 The water that flows in is dependent on
9 the low pressure drop. And the model I'm going to
10 show you, and it's consistent with the licensee and
11 vendor, it considers the pressure drop. So I have a
12 fixed head here. Depending on the core power level,
13 time and the event, that determines the steaming rate.
14 And that determines where the two phase level is. So
15 in the beginning of the transient very early the two
16 phase level is low. It will grow --

17 MEMBER WALLIS: It's not on top?

18 DR. WARD: In the beginning, that's right,
19 you've blown down the core. I mean, the whole core is
20 voided. Now you're refilling. This is early. And it's
21 slowly going to fill up. And I'm only going to be
22 able to get enough water in here that the loop
23 resistance will allow me. My ability to get water into
24 this core isn't any better than my ability to relieve
25 the steam around the loop.

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1 MEMBER WALLIS: And the boron comes in and
2 doesn't leave, so it just builds up?

3 DR. WARD: No. It just builds up. Right.
4 And that's why with cold side injection, that's why
5 cold leg breaks are worse for boron precipitation.

6 MEMBER WALLIS: You get some water in is
7 because there are other cold legs from that one, so
8 the water can get in?

9 DR. WARD: That's correct. Yes. There are
10 two other loops. So this is spilling and the other
11 one's keeping me full here. For this plant within
12 about 45 minutes to an hour, the two phased level is
13 up here above the bottom of the hot leg.

14 DR. BANERJEE: What's the partition
15 coefficient of boron between the steam and the water.

16 DR. WARD: What's the what?

17 DR. BANERJEE: Partition. I mean it's
18 partitioned, right?

19 MEMBER KRESS: It depends strongly on the
20 pressure and temperature.

21 DR. BANERJEE: I see.

22 MEMBER KRESS: Low pressure it stays
23 behind and high pressure it goes with the steam. It's
24 a variable

25 MEMBER WALLIS: With these pressures it

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1 stays behind.

2 MEMBER MAYNARD: Not much stays behind.

3 DR. WARD: We're assuming the steam does
4 not remove any of the boric acid nor is there taking
5 any credit for any entrainment. You look at the UPTF
6 tests, they show entrainment for about the first 15
7 minutes. For every pound of steam you're producing,
8 you're taking 2 or 3 pounds of liquid out. So you're
9 not going to build up very fast at all in the first 45
10 minutes. But that's neglected as well.

11 I mean so basically what I was going to
12 say, if you want steaming in the core and I fill the
13 vessel up, I'd have water here. But since I had void
14 in it and if the loop pressure drop isn't a
15 consideration, I'm going to swell up into the hot leg.
16 And I'll probably swell -- I won't swell the two phase
17 level any higher than within maybe a half of foot to
18 the top of this hot leg because the steam's got to get
19 out and it's going to pressurize. And you're going to
20 sit there concentrate.

21 Now, they don't take credit for the volume
22 above the bottom of the hot leg. They're just taking
23 credit for the mixing volume here, the core and half
24 of lower plenum. And the void fractions coming off
25 the top of the core early in the event throughout to

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1 about 6 hours is anywhere from 80 to about 65/70
2 percent. So it's pretty high. There's not much liquid
3 in this region hardly at all. I mean, it's very hard.
4 The void fraction, a very healthy steep gradient from
5 zero to 70/80 percent at the top of the core.

6 MEMBER WALLIS: I asked the question
7 previously, when you begin to get very high
8 concentrations of boron, doesn't that change the
9 formability and the drift flux and all that kind of
10 thing?

11 DR. WARD: Yes, i think it does.

12 DR. BANERJEE: I probably does.

13 DR. WARD: Yes. I mean --

14 MEMBER WALLIS: But that would make a
15 difference to the carryover.

16 DR. WARD: What I did in sensitivity
17 studies, you saw the Waterford report in there.

18 MEMBER WALLIS: Yes.

19 DR. WARD: I varied the drift velocity by
20 a plus or minus 25 percent. And, I mean, I'll show
21 some precipitation times. But when you're
22 precipitating out around 6 to 8 hours and in reality
23 you're really not going to get there until about 15,
24 14 or 15 hours and that's where this plant's at. And
25 I'll show you why that is.

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1 A change of 25 percent in the drift
2 velocity is probably not going to make much
3 difference. I mean, if the drift velocity goes down,
4 then I'm going to swell more, I'm just distributing
5 the liquid and steam over a larger volume. I still
6 got the same amount of liquid.

7 MEMBER WALLIS: The question we raised,
8 which I don't think was every answered, you know when
9 you boil down something like maple syrup it's just
10 like boiling water. But when you get it up to the
11 point where it's strong enough, it boils like milk.
12 It's overflow and go all over the kitchen because the
13 foaming --

14 DR. WARD: If it foams --

15 MEMBER WALLIS: It doesn't break. It
16 just--

17 DR. WARD: I don't think the BACCHUS test
18 showed that, but -- Yes but I mean those are good
19 questions. But what we have done, and I mentioned this
20 to you the last time we talked -- you had a lot of
21 questions --

22 MEMBER WALLIS: Yes, but answers --

23 DR. WARD: And you've had a lot of good
24 questions today, and you haven't got all the answers.
25 And I don't know all the answers because I want to

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1 know the answers to them, too.

2 We sent a letter out about 8 months ago,
3 about a 15 page letter with about 20 or 30 questions
4 asking what's the effect of boric acid on drift
5 velocity, what's the effect on viscosity, surface
6 tension, show us what the concentration profile is
7 across the core, what's the effect of adding debris in
8 here, how does that effect the concentration?

9 MEMBER WALLIS: Was this all to Beaver
10 Valley?

11 DR. WARD: All those questions are in
12 there. And we are --

13 MEMBER WALLIS: Is this to Beaver Valley
14 or is this a generic question to the industry?

15 DR. WARD: It's not the strict sense
16 generic letter issue. What we've done is we've sent a
17 letter to all the vendors asking them to answer this
18 question.

19 MEMBER WALLIS: Okay.

20 DR. WARD: And address these model
21 concerns--

22 MEMBER WALLIS: So then you'll report to
23 us on what happened some day?

24 DR. WARD: And we will.

25 MEMBER WALLIS: Okay.

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1 DR. WARD: But I haven't heard anything
2 yet. I know they're working on it. I think they're
3 still digesting it. And I think they're planning to do
4 calculations, experiments or whatever. And so when
5 that's done, then we will come and present that to
6 you.

7 MEMBER WALLIS: Okay. Good. Thank you.

8 DR. BANERJEE: A couple of these questions
9 clearly can be answered fairly easily, viscosity
10 surface --

11 DR. WARD: Sure. Sure.

12 DR. BANERJEE: But the drift velocity is
13 more difficult. And I guess maybe the people at MHI
14 would know the answer to that.

15 MEMBER WALLIS: But does it boil over? We
16 just need to put it on the stove in your kitchen and
17 wait.

18 DR. BANERJEE: Well, that's a good way to
19 do it, too.

20 MEMBER SIEBER: Another way.

21 MEMBER WALLIS: Well, it's best to do it
22 outside on the grill or something.

23 DR. WARD: Yes, right. Right. Well, those
24 questions have been asked. And again, when we've had
25 meetings with -- when we get some of the results from

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1 all these questions, then we'll be happy to share them
2 with you.

3 MEMBER WALLIS: If I buy some borax and
4 dissolve it in water in my kitchen, can I boil it and
5 see what happens?

6 DR. WARD: Sure. I mean --

7 MEMBER WALLIS: Would that be realistic?

8 DR. WARD: Well, there was a test done,
9 and I probably shouldn't -- you know, I'm not sure if
10 I should mention it or not.

11 MEMBER WALLIS: Well then don't.

12 DR. WARD: So I can't. But if you took a
13 plexiglass vessel and pumped borated water into it, an
14 electrically heated core and you pumped it in at the
15 RWC concentration of roughly -- now they're up around
16 2600 ppm, and if you took pictures of it you would see
17 because if the water's cold coming in the lower
18 plenum, you see some crystallization even on the
19 surface. But the test would probably show mixing
20 throughout the entire lower plenum and core. And
21 there'd be a gradient in there. But once it
22 precipitates, when you hit that limit based on
23 whatever pressure you're at, it's probably going to
24 look like you filled that whole thing up with salt.
25 Lower plenum core and upper plenum is going to be

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1 looks like full of table salt, crystals.

2 But, you know, there may be some worm
3 holes through it. You know, there are some cooling
4 channels that may be there. But that's probably
5 what's going to happen.

6 But what I'm going to show in this
7 calculation so we don't get anywhere near that --

8 MEMBER WALLIS: But it would be slurry
9 cool. It would be slurry cooled. It won't freeze up
10 solidly?

11 DR. WARD: Yes. Probably.

12 But I want to show you. hopefully we
13 shouldn't get anywhere near there. And there's enough
14 margin to accommodate. We don't feel that there's
15 answers here, we just want to make sure the industry
16 is doing everything consistent. They're not using a
17 1.0 multiplier. They'll all using appropriate mixing
18 volumes. They're taking credit for the void fraction
19 in there instead of assuming it's full of liquid, and
20 they're not assuming the whole mixing volume is this
21 size from time zero on, because it grows. So let's do
22 it right. And they are doing that. And they're
23 starting to do that now.

24 So let me just go over some of the
25 assumptions. I've already discussed it. We're only

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1 taking credit for half -- they're only allowed to take
2 credit for half the mixing volume in the lower plenum.
3 The core and the upper plenum, they choose to just
4 credit the volume below the bottom elevation of the
5 hot leg.

6 Now this was done during the Waterford
7 review, and you'll remember that. I did some
8 calculations. Compared my model to that. And as I
9 recall, it's been a while since I looked at it, the
10 reason why we did this is because since it's an
11 average concentration, it more closely tracked the
12 concentration near the top half of the core instead of
13 some lower average. So they're only allowed to take
14 credit for half of the lower plenum. And I think there
15 was some mixing in the upper plenum, too. But we
16 predicated the precipitation time within an hour. So
17 for a crude model like that, it's probably not too
18 bad.

19 We're using the 1971 ANS decay heat
20 standard with an additional 20 percent. It's like the
21 plant's operating at 20 percent more power.

22 The mixing volume is calculated as a
23 function of time. The higher the steam rate, the
24 slower the growth of the two phase level and a mixture
25 of volume in the vessel.

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1 Now this is not a model assumption, but I
2 just wanted to point out that the source
3 concentrations for this plant are 2600 ppm. And
4 again, the cold leg break is limiting for
5 precipitation.

6 What you want to do --

7 DR. BANERJEE: 29.27 percent or what?

8 DR. WARD: That's at 14.7 -- that assumes
9 the pressure in the upper plenum is 14.7.

10 DR. BANERJEE: But it must include the
11 boiling point.

12 DR. WARD: That's the boiling point at
13 14.7 with boric acid in there.

14 DR. BANERJEE: So what's the --

15 DR. WARD: The upper plenum pressure is
16 going to be more -- upper plenum is going to be more
17 like 20 or 25 pounds pressure. So the precipitation
18 limit is not going to be 29. It's probably going to be
19 more like 32/33.

20 And now our additives in there that will
21 jack it up to about 40 percent. But we're going to
22 assume -- the licensee assumed conservatively 29
23 percent.

24 Now hot leg break. I guess I don't need
25 to -- if you have a hot leg break, clearly during the

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1 injection phase --

2 MEMBER WALLIS: Flushes it down.

3 DR. WARD: You're going to flush this
4 thing fairly quickly because you're going to fill it
5 up. And once the two phase level in the vessel gets
6 above the bottom of the core, it's going to start
7 flushing. AS a matter of fact, it's going to have
8 positive flow through there and I don't think they're
9 going to build that much boron at all. So that's why
10 hot leg breaks are clearly not the thing you want to
11 look at.

12 Now, if you take that model, and it's the
13 same model that I described last time and it's
14 documented in the Waterford report. So if you want to
15 see the physics of the model, it's pretty simple. It's
16 hydrostatic balance against a loop pressure drop where
17 the drift phrase model calculates a two phase level.
18 And that drift flux model is compared against test
19 data that I've shown you on AP 1000. But it's
20 documented again in that report. So if you want to
21 see anything more on that, you know, feel free and I'd
22 be happy to come over and explain it in some detail.

23 I want to show you the calculation that I
24 did compared to the Westinghouse calculation. And
25 this is the concentration as a function of time. You

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1 can see that the Staff model predicts the Westinghouse
2 calculation, and I used this decay heat, their sump
3 concentration as a function of time which they
4 calculated. Basically used the same assumptions in
5 the calculating a precipitation time, which is within
6 15 minutes.

7 DR. BANERJEE: Based on the same volume?

8 DR. WARD: Based on the same mixing
9 volume. That's half below plenum, that's the core.
10 And only the volume in the upper plenum below the
11 bottom elevation of the core.

12 Now they could have taken credit for the
13 volume in the upper plenum adjacent to hot leg because
14 the level swells up to there within about an hour,
15 hour and a half and it's going to sit there near the
16 top of the hot leg. So there's an additional 200
17 cubic feet.

18 The lower plenum in this plant's about 750
19 cubic feet. So we're getting about 325 in the lower
20 plenum. Let's see, the core area as I recall is 42
21 square feet, the height's 12½ feet. So you've got
22 about 400 in the core and another 200 in the upper
23 plenum. And in the hot leg, they've got about another
24 200 cubic feet, but that's being neglected.

25 And remember, the steam doesn't carry it

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1 away. There's no entrainment. The upper plenum
2 pressure is 14.7. I'm not taking credit for
3 additives. I'm up here if I take credit for the
4 additives. I know we don't like to extrapolate, but
5 gee, we're talking --

6 MEMBER WALLIS: Ten hours.

7 DR. WARD: -- 10 hours or more. And
8 they're switching at 6 hours. I guess they're
9 starting at five. I'm sorry. So I mean there's
10 clearly 4 or 5 hours there of margin relative to
11 these.

12 MEMBER SIEBER: Volume of the core is not
13 the product of the physical dimensions because the
14 core itself occupies about half that space, right?

15 DR. WARD: That is the free space. That's
16 the free area.

17 MEMBER SIEBER: That's the --

18 DR. WARD: That's in between the rods and
19 the --

20 MEMBER SIEBER: Okay.

21 DR. WARD: Yes. It was the core flow
22 area. Okay.

23 That's a conservative calculation. I mean,
24 it's bounding.

25 Now what I want to do before I talk about

1 boron precip for small breaks, let's talk about the --
2 yes, blurry. Can you see that okay?

3 MEMBER SIEBER: Yes. Better than the
4 other one.

5 DR. WARD: Okay. The old technology
6 works.

7 When Veronica Klein and I looked at the
8 spectrum, we noticed they only looked at integer break
9 sizes. And if you look 1, 2, 3, 4, 5, 6 inch diameter
10 breaks, you find the area is .0055, .02, .05, .09,
11 .14; there's a pretty wide range there. And typically
12 for small breaks the limiting break is usually in the
13 .05 square foot range, somewhere in here and it's
14 typically a break that's controlled entirely by HPSI
15 flow, which means you find a break size with a system
16 depressurizer and it hangs up just above 600 pounds.
17 The HPSI flow doesn't put as much flow in as an
18 accumulator so it's going to uncover and then slowly
19 recover. And typically that's the worse small break.

20 For this plant the accumulator comes on
21 during that range. We asked them to do a more
22 detailed spectrum analysis, and you saw that plot.
23 Maybe quarter inch. They went every quarter inch
24 between 2 and 3 and 3 and 4 and found out that breaks
25 between 2 and 3 could be more limiting. The worse

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1 break turned out to be a 2.75 inch break compared to
2 the original analysis submittal of 1759. Now this is
3 not one-to-one because I think the 1917 degree F PCT
4 is a time in life study for oxidation. I think the 2½
5 inch break was worse because although the peak didn't
6 quite get up, it was uncovered longer so the
7 oxidations were like 13.42 percent. But basically
8 what this did looking at a more detail spectrum,
9 better identified the PCT. And when you got these
10 high power uprates, I've seen a plants with a
11 difference of .005 square feet, the PCT can increase
12 by 70, 80 degrees. So when you're getting p around
13 1900, 2000 if you want to make sure the margin by
14 Appendix K is there, then you need to do this. You
15 need to do a better calculation.

16 Now we did some calculations. Veronica
17 Klein and I did. Veronica did most of the
18 calculations.

19 DR. BANERJEE: This is by using your --

20 DR. WARD: This is RELAP5. No, this was
21 RELAP5. We had a deck. And we got it -- we might
22 have gotten from the licensee and we thank them for
23 that. They have been very cooperative in answering
24 all questions. In trying to understand their model,
25 I've even asked them to do some calculations so I can

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1 understand how their model behaves. And they answered
2 everything.

3 DR. BANERJEE: What is actually run here
4 for the RELAP5? Is it just the core region?

5 DR. WARD: No. This is the entire system.
6 It's your full blown RELAP5 model, okay. Vessel, each
7 loop. Now we've got 24 cells in here. Better track
8 the two phase level. And also put a hot bundle in
9 there with 24 cells in it with a hot rod in it.

10 DR. BANERJEE: And this is the low
11 pressure long term --

12 DR. WARD: No, this is short term. This
13 was for PCT. No, no. The boron precip stuff is --

14 DR. BANERJEE: But you don't continue this
15 into the low pressure?

16 DR. WARD: Yes. I ran this all the way out
17 to 8 or 9 hours to show refill. And I'll get to that
18 on the long term part. We ran this for short term to
19 look at PCT. We also ran it to show for small breaks
20 where you can't the pressure down low enough to flush
21 the core, but you can refill the core or resubcool it,
22 reestablish single phase natural circulation and
23 disperse the boron. It was run for that. I'll show
24 you some of those.

25 DR. BANERJEE: Yes, how does it behave at

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1 low pressure?

2 DR. WARD: Well, great. I mean ask
3 Veronica. I mean, Veronica never came in my office
4 once and said "Damn code bombed again on properties."
5 Never said that once. Run these cases up two hours.
6 We ran .5, .75, 1 all the way up to one square foot.
7 We looked at breaks on the top of the pipe because the
8 flube seals would fill up and potentially depress the
9 core. And we also looked at side breaks. And we found
10 that the most limiting break was between these 2 and
11 3 inch range. A little different break because
12 they're different critical flow models. But we
13 basically beat it to death.

14 And we ran these tiny breaks half an inch,
15 1, 2, 3, 4 out 30,000 seconds.

16 And running with a .05 second time step,
17 the case runs in two hours.

18 MEMBER WALLIS: You didn't use TRAC?

19 DR. WARD: No. I didn't have an input deck
20 for it.

21 DR. BANERJEE: But I thought this was
22 seamless now, conversion from a RELAP5 deck to TRAC?

23 DR. WARD: Not quite.

24 DR. BANERJEE: Little seams still there?

25 DR. WARD: Yes, there's some bugs in it,

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1 you know. The control system you've got to develop.
2 They're not quite the same. You know, the RELAP5
3 input is a little different, but they're getting
4 there. Not quite there yet.

5 DR. BANERJEE: Okay.

6 DR. WARD: They're working feverishly on
7 it.

8 So I guess I've already said that. So
9 basically we confirmed the worse break, ran it 14
10 kilowatts per foot, I think it's a little higher at
11 the extended power uprate value. And what I want to
12 do is show you this break between 2 and 3 inches.

13 And the thing I want to point out is the
14 accumulators. The accumulators are keeping the PCT
15 down below 2000 degrees. And you can see they're
16 coming on here. So the system pressure then rises.
17 They cut back off because it fills the core back up
18 and so there's more energy addition, the pressure goes
19 up. And there's a balance between energy addition and
20 break flow. And so you don't get a huge deluge but
21 it's enough to turn that temperature over. So the
22 accumulators are really controlling PCT here. So if
23 anybody says accumulators are there for large breaks.
24 No, small breaks. That's why they're there. That's
25 why they're important.

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1 I'm not going to bore you with the
2 results, I just thought I'd show you a PCT plot. And
3 there's 24 cells in the core, so the peak, the peak is
4 in the top four cells. Temperature is around 1900
5 degrees.

6 DR. BANERJEE: When do the accumulators
7 kick in that?

8 DR. WARD: The accumulators kick in right
9 about here and then they deliver enough flow and they
10 turned it over right here. The accumulators are
11 kicking in right about here.

12 MEMBER WALLIS: That's 5 or 6 hours.

13 DR. BANERJEE: And what are those two
14 curves?

15 DR. WARD: Those are two different axial
16 slices. This is cell 22. That's two cells from the
17 top of the core. And this is cell 20. It's 24 cells
18 in that. That's in the hot bundle. So if you want to
19 capture the shape and the void distribution at two
20 phase level, you really need -- I wanted to make sure
21 we had enough detail in there to capture it.

22 DR. BANERJEE: These are the hottest
23 areas?

24 DR. WARD: This is the hot bundle. Right.
25 The hottest bundle in the core and the hot rod with

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1 the 1400 kilowatts per foot approximately 2 or 3 feet
2 from the top of that core.

3 Now remember this is Appendix K. This is
4 20 percent more power than is really there. If we
5 rerun this with 1.0 multiplier, this temperature is
6 going to come down here. It's just like increasing
7 the HPSI flow by 20 percent. That's huge. So it's a
8 pretty big conservatism. That's probably the
9 conservatism.

10 And we can skip the next one. It's just
11 another break size and it just shows you the
12 accumulators are controlling PCT here.

13 I'm only going to mention this quick. If
14 you look at those slides, you'll see a first peak
15 here. There's an early CHF condition. Westinghouse
16 didn't calculate it. I did. It's about 2000 degrees.
17 And I'm not quite sure. We haven't really figured out
18 what's causing it, but my suspicion it's a combination
19 of two things. I'm assuming a reactor trip at the
20 time you get -- I'm assuming a loss of offsite power
21 at the same time you would get a reactor trip on a low
22 pressure during that event. What that does is it says
23 the -- start coasting down and I got about a 2 second
24 delay before rods go in, so I've got two to three
25 seconds before the rods in far enough where I'm

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1 generating full power and I'm voiding that hot bundle,
2 very quickly and rapidly, and I get a heat up.

3 MEMBER WALLIS: And you said Westinghouse
4 didn't calculate them?

5 DR. WARD: They made the same assumption
6 in their model tripping it at the same time and
7 they're not getting a first peak.

8 DR. BANERJEE: They used NOTRUMP, right?

9 DR. WARD: They're using NOTRUMP, I'm
10 using RELAP. Now, I've got a single hot bundle
11 channel with cross flow.

12 DR. BANERJEE: How far into the transient
13 is this?

14 DR. WARD: It's right at reactor trip.

15 MEMBER SIEBER: Two seconds.

16 DR. WARD: It's two seconds in. Once I
17 get reactor trip --

18 MEMBER WALLIS: So it still meets the
19 regulation?

20 DR. WARD: It meets the regulation. The
21 bottom line is it's still below 22. I've never seen
22 a first peak much over 2000. It's usually anywhere
23 from 1400 to 2000 degrees. But I only mention it, you
24 know, we've been talking to each other. We want to get
25 to the heart of it and figure out what -- there's

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1 probably differences in the model. It could be input.
2 You know, I'm not sure. But I just wanted to mention
3 it because it's there and however even if we're
4 conservative in the resistance and the way we modeled
5 it, it's still -- the PCT is still less than 2200.

6 DR. BANERJEE: Your model is a two fluid
7 model whereas theirs in some form is always a mixture
8 model of sorts?

9 DR. WARD: Yes. It's drip flux approach.

10 DR. BANERJEE: Yes. So you cannot decouple
11 of the phases which you can?

12 DR. WARD: Right.

13 DR. BANERJEE: So they're bound to move --

14 DR. WARD: Right. Yes.

15 So anyway, what we'll do, we'll follow up
16 with this. If it looks like we need to pursue this
17 farther, then we will. But I think we probably, we'll
18 be able to resolve this once we have the time to
19 devote to it. More important things were long term
20 cooling, operator actions and behavior.

21 Now what I'll do is get into the small
22 break. And as I said, small breaks pressure can hang
23 up 1 or 200 pounds for these tiny leaks for long
24 periods of time. And the pressure remains too high
25 and you can't flush. So what do you do? You've got to

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1 reduce the pressure to low enough to flush it or cool
2 down early enough and fast enough within your cool
3 down tech spec limit and refill this thing and
4 resubcool it.

5 And this was an open item identified in
6 the SER, but we're very close to getting closed here.
7 The licensee has done their calculations. I haven't
8 seen them yet, but once I see them and I can see that
9 they've got essentially the same response that I did,
10 then that will be a closed door. But --

11 MEMBER WALLIS: This comes to the full
12 Committee when it's all going to be sorted out?

13 DR. WARD: Yes. Yes.

14 MEMBER WALLIS: Yes?

15 DR. WARD: Yes, it should.

16 MEMBER WALLIS: Next week?

17 CHAIRMAN DENNING: That's next week.

18 DR. WARD: Yes, it should. They've got the
19 calculations all finished, I just haven't seen them.
20 I just want to -- I have convinced myself that this
21 works. And I'm comfortable with it. I understand it,
22 did the calculations.

23 MEMBER WALLIS: But it's up to them to
24 show you.

25 DR. WARD: But it's up to them to do it

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1 and it's up to them to make sure that it works with
2 their model. And they have said that they're getting
3 the same response that I've got for these breaks.
4 It's for the breaks they can't flush, the refilling
5 for the bigger breaks, they're depressurizing and
6 they're flushing the core.

7 DR. BANERJEE: Tell us the differences
8 that were there before you started to rationalize it.
9 What were you seeing and what were they seeing?

10 DR. WARD: Well, I wasn't seeing anything
11 from them. I wanted them to do this. There wasn't any
12 analysis of this at all. This was a question I had,
13 hey, you guys got to look at small breaks, too,
14 because you've either got to cool it down and flush it
15 or you got to refill it. And I want to see those
16 calculations. And they did that.

17 DR. BANERJEE: Okay.

18 MR. HARTZ: Yes. This is Josh Hartz of
19 Westinghouse.

20 Dr. Ward did some hand calculations that
21 cast some concern on the depressurization aspects
22 under small break LOCA long term cooling. We have
23 since gone off and done some runs in NOTRUMP space to
24 demonstrate you can get down to a low pressure to the
25 point where you can provide RHR flow to mitigate the

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1 boron precipitation here in a timely manner.

2 And also in speaking for Dr. Ward, he has
3 since done RELAP calculations which basically show the
4 same thing. And we're in the process of validating
5 those calculations and they'll be done within the next
6 few days, the official review of them.

7 DR. WARD: I'm going to show you the
8 results of a 1, and a 2 and a 3 inch break in the cold
9 leg. And you can boil for a while here.

10 This is RCS pressure versus time and you
11 can see the smallest break here is the 1 inch break.
12 It hangs up on a pressure plateau. That's because the
13 break is not big enough to depressurize the system.
14 You need heat removal through the generator. So a
15 delta T will develop between the primary and the
16 secondary. You are condensing steam here. You are
17 refluxing. And it's holding the pressure above the
18 secondary side, which is probably around 1100,
19 somewhere, a 1000. At one hour open the atmospheric
20 dump valves, cool this plant down. And cool down.
21 And then at about a little over an hour and a half,
22 maybe just under two hours, you can see this little
23 blip there. And I should have blow this. I apologize.
24 But what happens here is it refills. And if I plot the
25 void fraction in the core, you will see it go up and

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1 it will go to zero right at this time.

2 Now, if I look at a little bigger break,
3 a 2 inch break --

4 DR. BANERJEE: Is there any core uncover
5 during that refluxing?

6 DR. WARD: Yes. For the 2 inch -- it's in
7 the short term. It's back. It's occurring back --
8 well, it would occur back in here. Now remember that
9 analysis that you saw for short term doesn't assume
10 any cool down. So if you cool down, you've probably
11 got to limit the amount of uncover and it's recover
12 fast. So the temperature is probably going to be a
13 little lower.

14 But we're looking at boron precipitation
15 and getting down here. And the procedure now says
16 cool this plant down at an hour. And so what that
17 does is the one inch refills at about 7,000 seconds.
18 Just under 2 hours.

19 The 2 inch, and see I stopped it after
20 refill. It refilled right here. So it's a little
21 bigger break, take a little bit longer to refill. But
22 it repressurized and it's resubcooled, void fraction
23 went to zero right here in the core.

24 And then I said let's run the 3 inch, what
25 happens with that guy. And, of course, he

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1 depressurizes a little faster because the break's big
2 enough to -- you get steam out the break and you
3 depressurize real early. But that refills out here
4 around 17,000 seconds. And you can see the void
5 fraction in the core go to zero right about there.

6 And if I look at a 4 inch or bigger, I'm
7 down below 100 pounds in the real low pressure range
8 where the high pressure pump is going to flush it.

9 DR. BANERJEE: Then let me ask you
10 something. You get significant periods of concurrent
11 flow here, right?

12 DR. WARD: Yes, that's right.

13 DR. BANERJEE: In your opinion how does
14 NOTRUMP calculate concurrent flow?

15 DR. WARD: Well, it looks at the junction
16 connected from the hot leg to the generator. And it
17 looks at the steam flow going up and it says if the
18 steam flow is greater than a JG that says no liquid
19 goes down, then it doesn't allow liquid to go down.
20 I think the drift velocity model is solved such that
21 if you're in that flooded region, only steam goes up
22 and no liquid will come out.

23 DR. BANERJEE: Can you get counter
24 currents.

25 DR. WARD: Yes, you can. If the steam

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1 velocity is low enough, you can have -- for this
2 transfer -- small breaks typically you don't see the
3 water hold up for these 2 and 1 and 2 inch breaks
4 because there's not enough steam flow. You're far out
5 in time. There's a large area there. So there's just
6 not enough of a flux to hold it up.

7 With these power uprates though, you asked
8 a good question. You're starting to see higher steam
9 rates. And they did see some hold up. And I saw that.
10 We asked them hey, what happens if you don't hold it
11 up, you let it drain out or carry it over. And Josh
12 did some calculations where he let it drain it out.

13 If you let it drain out, then the core
14 uncovers later and not as deep because it's in a lower
15 decay heat span. Because the code was calculating
16 some water hold up, once the core uncovered, you can
17 see once it got down to about 50 percent, 60 percent
18 uncover, the steam rate dropped off. The JG was too
19 low and liquid started to drain out. What it did is it
20 recovered the two phase level. But it turned out that
21 the early uncover, even with that slight recovery,
22 that's still worse than throwing it on the other side
23 or letting it drain out. Because what it does is it
24 throws the uncover out farther in time when the decay
25 heat is lower, so that's not as limiting.

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1 MR. HARTZ: Yes. Plus there was a little
2 bit of a extended period of two phase low quality
3 mixture coming out the break in the cold leg there,
4 which tended to drive mass loss up.

5 DR. WARD: Okay.

6 DR. BANERJEE: And RELAP5 isn't great at
7 this flooding calculation either. Because, you know,
8 the problem -- we can discuss it off line.

9 DR. WARD: Okay.

10 DR. BANERJEE: But it's long known that
11 the interfacial drag correlation has difficulties in
12 this region.

13 DR. WARD: Yes. Could be.

14 DR. BANERJEE: Way back --

15 DR. WARD: Yes.

16 So what this really says is it really
17 emphasizes operator action. I mean to control boric
18 acid you have to cool -- in order for this refill to
19 occur, you have to initiate a cool down at an hour.
20 And the licensee has agreed to emphasize or make sure
21 that it says start your cool down no later than an
22 hour. Because it's important to depressurize and get
23 the pressure down and flush it as early as -- you
24 don't want to sit there boiling for long period of
25 time because if you did, let's say a dump valve failed

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1 -- and that analysis I did I'm going to point out
2 there are four dump valves. I failed one of them and
3 I failed the HPSI part; that's a multiple failure
4 event and it still worked.

5 What this says is that they need to be
6 very aware of there are other depressurization
7 capabilities. And they have to PORVs as a backup.
8 Plus four dump valves. There's one on each generator
9 and then there's a common one on the main steamline
10 for both units. And they're a huge capacity.

11 So really what this says is the EOP
12 guidance is really important and the equipment you use
13 to cool down. And make sure that you can control
14 boric acid for small breaks is important. And all
15 they need to know is when the break opened and they
16 switched to simultaneous injection at 6 hours, that's
17 all they need to know about. But they need for small
18 breaks to be successful, you need to cool down no
19 later than an hour. If you're going to wait longer
20 then -- the scenario is going to change. The other
21 thing is you don't also caution -- there's going to be
22 a caution in there, I think this is part of their
23 training program. And if your boiling for extended
24 period of time, let's say you're out eight to ten
25 hours. And since the pressure in those cases is up

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1 pretty high, the precipitation limit is up like 50
2 percent. So the 6 hour doesn't apply. I can sit there
3 and boil for a while. But you don't want to do that
4 because if you get power back, you don't want the
5 operators crashing the pressure down when you've got
6 40 weight percent in the system. So it's important to
7 cool down and get this thing refilled and flushed as
8 early as possible.

9 And the calculations show that you can do
10 that. Even with a multiple failure event you can do
11 it. At least I'm convinced of it. And I think Josh
12 and Westinghouse has done the calculations to also
13 show that.

14 So the EOP, this review had done a couple
15 of things. It's identified a worse break. We got rid
16 of the integer break spectrum.

17 They were assuming all the loop blown.
18 Now that's not their approved model. Had them rerun it
19 again with only assuming the broken loop seal clears,
20 and that's what we approved. And they did in order to
21 compensate for the very high PCTs. Probably PCTs over
22 2200, they increased the accumulator pressure to 625
23 to keep it down around 1900. So from a safety
24 standpoint, that's a good thing to do. Now they'd
25 already increased the HPSI flow 5 percent. That's also

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1 from a safety standpoint a good thing to do.

2 But then the Staff calculations on boric
3 acid precipitation for small breaks also enabled us to
4 emphasize the need for the EOPs and have the operators
5 cool this thing down no later than an hour and be very
6 sensitive to the depressurization equipment that they
7 have. And not to inadvertently depressurize the
8 system if you for some reason boil for 8 to 10 hours.
9 And even if you're up there around 100 pounds to 200
10 pounds pressure, boiling for 10 or 15 hours, it's in
11 solution. You've got 55 weight percent for probably
12 a limit. But your accumulating too much boil. You
13 don't want to sit there too long. The emphasis is get
14 the thing down and get it refilled.

15 CHAIRMAN DENNING: I'm missing as far as
16 whether you made recommendations for EOP actions that
17 haven't really been implemented yet relative to this
18 timing of cool down?

19 DR. WARD: Right. The vendor needs to EOP
20 guidance that's consistent with their analyses that
21 shows in order to refill the system for these small
22 breaks, you need to initiate a cool down no later than
23 an hour. Don't boil for long periods of time because
24 you can get --

25 CHAIRMAN DENNING: You say "initiate a

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1 cool down." Where do you have to be when?

2 DR. WARD: Well, you start -- remember I
3 showed you the calculation. Right here. One hour.

4 This analysis, the refill for these breaks
5 and you flush this. It's based on cooling down at one
6 hour. If you come out here, I mean you're going to be
7 boiling for a longer time, you're going to build up
8 more boron. It's probably not a good thing to sit
9 there boiling for a long time building up a lot of
10 boron because you put yourself in a situation where if
11 you get power back out here and then you decide to
12 open the turbine bypass and crash -- let's say you
13 could crash the pressure down, you could cause a
14 precipitation. You don't want that to happen.

15 You want to cool it down. Start the cool
16 down early and get it refilled and disperse the boron
17 so you don't have these large amounts of boron in the
18 system.

19 MR. HARTZ: This Josh Hartz from
20 Westinghouse again.

21 The way the EOP guidance is currently
22 written this would occur. In fact, it would occur
23 sooner than that. What Len's analysis is showing that
24 if you start to cool down at one hour, the boron
25 precipitation concern as analyzed here really isn't a

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1 concern.

2 Estimates from the Operations folks show
3 that this cool down would actually start somewhere
4 between 30 to 40 minutes into the transient. And
5 that's the way the guidance is currently.

6 And Pete with his Operations experience
7 can maybe add something to this.

8 MR. SENA: Yes. This is Pete Sena. We ran
9 the Operations crews both units through simulated
10 small break scenarios, various spectrums of small
11 breaks, using existing EOP guidelines. And the crews
12 were able to initiate the cool down with the existing
13 network within 30 minutes.

14 I personally ran it and with one signal
15 operator, assuming one operator was incapacitated. And
16 the cool down was initiated within 24 minutes.

17 So with existing guidelines we can satisfy
18 the one hour requirement that Len has identified.

19 DR. WARD: A couple of other things here,
20 too, I'd just like to add.

21 There's some other depressurization
22 mechanisms that we didn't even account for. And one
23 would be using pressurization ox spray if the power
24 operator relief valves on the pressurizer were not
25 available. We did not credit that.

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1 And also for these smaller breaks which
2 don't depressurize, like I discussed earlier you do go
3 through a single and two phase natural circulation
4 period. Typically for these breaks that's on the
5 order of anywhere from 1,000 to 2,000 seconds. During
6 that time frame everything within the reactor coolant
7 system is homogenous. And so these boil off
8 calculations would really start after that mechanism
9 breaks down.

10 We assume that that starts at time equal
11 zero. And so if the calculations has truly took that
12 into account, the actual hot leg switchover time would
13 be extended well beyond what is being calculated here,
14 not accounting for that.

15 DR. BANERJEE: But the RELAP5 calculations
16 automatically should take natural circulation and
17 break down of natural circulation into account.

18 DR. WARD: They did. They did. They have
19 that in there. That's built it. That's built it.

20 DR. BANERJEE: So I mean that's
21 automatically taken --

22 MR. LASH: Yes, it's in there.

23 DR. BANERJEE: --into account then.

24 DR. WARD: Right. You're right. That's
25 correct.

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1 MR. HARTZ: Well, they do for the
2 depressurization aspects, but for the boric acid
3 precipitation calculations they do not because it's a
4 different model.

5 DR. WARD: Yes, that's a different model.

6 DR. BANERJEE: But you could incorporate
7 boric acid into your -- as a scale of field, right?

8 DR. WARD: You could. And then you get
9 diffusion problems. You know, you got to make sure
10 that -- all over these cells.

11 DR. BANERJEE: Because of your --

12 DR. WARD: Because of the first order --
13 difference on the --

14 DR. BANERJEE: On the cells.

15 DR. WARD: You know, so I got to go
16 through and got to do a third order and then I got to
17 a put -- boy, that's a pain in the you know what.

18 DR. BANERJEE: Yes. So the scale equation
19 would have to be solved --

20 DR. WARD: That's right. That's right.
21 Right.

22 CHAIRMAN DENNING: You done?

23 DR. WARD: Yes, I'm done. So I guess I
24 don't -- unless you have any questions.

25 CHAIRMAN DENNING: Thank you.

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1 DR. WARD: Looks fine.

2 DR. BANERJEE: You do that in any case,
3 you know.

4 DR. WARD: Yes.

5 DR. BANERJEE: You could with a lot of
6 these issues?

7 DR. WARD: I could, yes.

8 DR. BANERJEE: It's not such a big deal.

9 CHAIRMAN DENNING: And now we're going to
10 have a discussion of containment from NRR.

11 To the extent that there is some
12 repetition, go quickly.

13 MR. LOBEL: Yes, there's a lot of
14 repetition.

15 Good afternoon. My name is Richard Lobel.
16 I'm a senior reactor systems engineering in the Office
17 of Nuclear Reactor Regulation. I'm here today to
18 discuss the Staff review of the FENOC proposal to
19 convert the Beaver Valley Unit 1 and Unit 2
20 containments from sub-atmospheric to atmospheric
21 containment designs.

22 The licensee performed the analyses to
23 support the containment conversion at extend power
24 uprate conditions. So the Staff's review of their
25 containment conversion also serves as the review of

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1 the extended power uprate.

2 A lot of what I was going to say has
3 already been discussed, so I'll try to go through it
4 or skip parts of it.

5 Next. Okay.

6 February 6, 2006 there was an NRC letter
7 to FENOC that approved the conversion of the Beaver
8 Valley Unit 1 and Unit 2 containments from sub-
9 atmospheric to atmospheric. And as part of that
10 proposal, part of the original proposal the licensee
11 included consideration of extended power uprate and
12 the Unit 1 steam generator replacement. Also the
13 licensee used the new analysis method, MAAP-DBA.

14 Next slide.

15 Beaver Valley units aren't the first power
16 plants to convert from a sub-atmospheric to an
17 atmospheric containment. Millstone Unit 3 is a 4 loop
18 Westinghouse designed reactor that was originally
19 licensed as a sub-atmospheric containment in 1986 and
20 in 1990 the licensee for Millstone proposed converting
21 from a sub-atmospheric containment to a higher
22 pressure but still with a vacuum, but the design basis
23 was changed to that of an atmospheric containment,
24 which is pretty much what Beaver Valley has done. And
25 the staff approved the Millstone Unit 3 proposal in

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1 January of 1991.

2 I think I'll skip this one. The licensee
3 already talked about the pressure ranges, that they're
4 increasing the pressure in the containment but it'll
5 still be operated from 12.8 psia to a very slight
6 vacuum. The licensee added a lower temperature limit
7 in the tech specs also that limits the mass of air in
8 the containment for a given pressure that's important
9 for the pressurization calculations.

10 Next slide. Let me just say that this is
11 the sub-atmospheric containment design bases which
12 were the design bases for the Beaver Valley
13 containments before the conversion. And the design
14 bases that are italicized are the ones that changed.

15 For sub-atmospheric containment the
16 requirement is to depressurize after a LOCA in one
17 hour and once depressurized to stay sub-atmospheric
18 for the rest of the accident. And that has a direct
19 impact on the dose calculations once the reactor is
20 depressurized again, they don't have to assume leakage
21 from the containment for dose calculations.

22 For the atmospheric containment design,
23 the other design bases remained the same, but the ones
24 of concern, the sub-atmospheric containment, were
25 replaced by one that says that the containment

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1 pressure should be less than 50 percent of the peak
2 within 24 hours. And the reason for that is that
3 helps in the dose calculations because when the
4 pressure is less than 50 percent, the guidance for
5 dose calculations states that the containment leakage
6 can be reduced by half after 24 hours.

7 CHAIRMAN DENNING: What do you mean
8 "minimum containment pressure greater than 8 psia."
9 It's just at that initial time when they need credit?

10 MR. LOBEL: For the atmospheric
11 containment -- no, they calculate a peak pressure and
12 then they demonstrate that within 24 hours the
13 pressure is reduced to 50 percent of that peak
14 pressure.

15 CHAIRMAN DENNING: Your fifth bullet right
16 there.

17 MR. LOBEL: Oh, that's really a
18 requirement for reverse pressure on the containment
19 that the pressure on the outside of the containment
20 could be larger than the pressure inside the
21 containment. And --

22 MEMBER WALLIS: Is it collapsing the
23 containment you're worried about?

24 MR. LOBEL: Yes. And there's a structural
25 requirement for that. And that's demonstrated by

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1 assuming an inadvertent actuation of the containment
2 sprays and that the pressure won't go down below 8
3 psia.

4 CHAIRMAN DENNING: But clearly you'd have
5 to lose an awful lot of air for that to happen in this
6 containment?

7 MR. LOBEL: Well, you start with a low
8 pressure and then you make very conservative
9 assumptions about the temperature of the sprays and
10 that kind of thing.

11 CHAIRMAN DENNING: Okay.

12 MR. LOBEL: It's a very conservative hand
13 calculation.

14 The large break LOCA I think you've pretty
15 much gone through, or the licensee pretty much went
16 through with that. Let me just say that the
17 calculations for the mass and energy release were done
18 with NRC approved Westinghouse methods for less than
19 one hour. For greater than one hour the mass release
20 was calculated with the same NRC approved Westinghouse
21 methods. The energy was calculated with the MAAP-DBA
22 code.

23 We had some questions about separating the
24 calculation of the mass and the energy between two
25 separate codes. So Veronica Klein, who is still here,

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1 did some calculations for us with the RELAP code that
2 essentially verified that we got almost the same
3 results the licensee did with separating the two
4 calculations. And so we found that their approach was
5 satisfactory.

6 You've already seen the LOCA results. I
7 won't go through that again.

8 For the main steamline break, the mass and
9 energy release calculations were done with
10 Westinghouse approved methods. The licensee modeled
11 the replacement steam generators, the cavitating
12 venturies. Since it's difficult to tell what size
13 break and what power level they're limiting for main
14 steamline break, the licensee did a spectrum of breaks
15 and power levels. And made conservative assumptions,
16 the -- failure and other conditions that maximize the
17 inventory in the steam generator and the stored energy
18 in the steam generator.

19 One of the important parameters from the
20 main steamline break calculation is the liner
21 temperature. The LOCA gives the peak containment
22 pressure, the main steamline break is the highest
23 temperature. The acceptance criterion for the
24 containment liner was 280 degree. And the licensee
25 calculated temperatures lower than that with

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1 conservative assumptions. For instance, the heat
2 transfer coefficient between the containment
3 atmosphere and the liner was multiplied by a factor of
4 4 that's consistent with the Standard Review Plan.

5 Now for over pressure and NPSH. The
6 Standard Review Plan Section 6.2.2 for sub-atmospheric
7 containment allows credit for containment accident
8 pressure for available NPSH during the injection phase
9 of the LOCA. At the pre EPU power level for the sub-
10 atmospheric containment Beaver Valley Unit 1 credits
11 containment accident pressure calculating the
12 available NPSH for the recirculation spray pumps and
13 the low head injection pumps. And this was part of the
14 original licensing bases.

15 At the pre-EPI power level in the sub-
16 atmospheric containment Unit 2 doesn't credit
17 containment accident pressure. At the extended power
18 uprate conditions conversion on the atmospheric
19 containment, the containment accident pressure is
20 credited for Unit 1 for the recirculation spray pumps
21 not for the low head safety injection pumps. That's
22 based on changing the timing of the actuation of the
23 low head safety injection pumps.

24 Unit 2 at extended power uprate with the
25 containment conversion still doesn't need credit for

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1 containment accident pressure.

2 Let me see. I think they went through the
3 basic reasons. Basically for Unit 1 the recirculation
4 spray pumps start at a time when the level in the sump
5 is still relatively low and the temperature of the
6 sump water is relatively high and due to the placement
7 of the pumps in Beaver Valley 1, that's what requires
8 credit for containment pressure. And we queried the
9 licensee about what would happen if you did a
10 realistic calculation and not a conservative
11 calculation. And they say that due to those factors
12 they would still need credit for containment accident
13 pressure.

14 CHAIRMAN DENNING: I wasn't sure I heard
15 that earlier. Is that basically the position of
16 Beaver Valley that for realistic calculation with
17 uncertainties, not suggesting that you would do that,
18 but is that your feeling that -- did you hear that
19 fifth bullet?

20 MR. LOBEL: We asked that question in a
21 formal RAI.

22 CHAIRMAN DENNING: In a RAI. So it get a
23 formal answer.

24 MR. FREDERICK: Ken Frederick.

25 In looking at a better estimate analysis

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1 the parameters that we can vary towards more best
2 estimate do not directly impact the sump temperature
3 to a degree where we could get rid of the requirement
4 for containment over pressure. There is some benefit
5 there, but it's not enough to get rid of the
6 requirement.

7 CHAIRMAN DENNING: Thank you.

8 MR. LOBEL: Next.

9 This is similar to the curve that was
10 shown before, and it's a curve for the worst case of
11 the containment pressure actually in terms of
12 overpressure versus the pressure that's required for
13 adequate NPSH for the inside and outside recirculation
14 spray pumps.

15 Again, this is in terms of overpressure so
16 you're looking at their definition of overpressure
17 which is the calculated containment pressure above the
18 initial containment pressure.

19 And you can see that this is for the first
20 case, that they don't need the credit for a very long
21 time and there is margin to a conservatively
22 calculated containment pressure.

23 The difference between the peak pressure
24 in this case and the minimum pressure is really less
25 than it was last time I was here talking about Vermont

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1 Yankee. There was a lot larger difference. But the
2 licensee submittal was very good with respect to
3 talking about the input parameters that went into this
4 and sensitivity studies they did. And there's a table
5 in the Jun 2, 2004 letter, it's table 4.3 where they
6 have a list of the significant variables and
7 sensitivities that they've determined for the
8 different cases and for NPSH they assumed values that
9 were in the most adverse direction for calculating
10 NPSH.

11 So judging from that, we're convinced that
12 the calculation is conservative for a minimum
13 pressure.

14 The next curve you've also seen before,
15 and I think that had a pretty good explanation so I
16 won't go through that again. But, again, I think the
17 important point is in terms of containment integrity.
18 For the largest assumed hole between the inside and
19 the outside of containment, the largest penetration
20 that connects the inside atmosphere to the outside
21 atmosphere if I assume that that's open, I still
22 maintain some NPSH margin.

23 Next slide.

24 There is a 1977 report which was submitted
25 to the NRC where there was some testing of a

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1 recirculation spray pump for North Anna Unit 2. You
2 saw the NPSH curves for it before. And the central
3 point, again, was that this pump was tested in
4 cavitation at different levels and then run for half
5 an hour at a significant amount of cavitation well
6 below the 3 percent usual required NPSH value. And
7 there was essentially no wear and no damage to the
8 pump.

9 So in conclusion for this part, the Staff
10 accepted the licensee's proposed credit for
11 containment accident pressure in defining available
12 NPSH for the recirculation spray pumps based on
13 several reasons.

14 First, containment integrity is assumed
15 for postulated designed bases accident, in particular
16 as I've said before here, Appendix K permits the use
17 of conservatively minimized containment pressure in
18 determining peak cladding temperature and oxidation
19 limits. And also offsite and control room dose
20 calculations assumed containment leakage at -- which
21 is a very large leakage value of containment that's
22 specified in the technical specifications. And that
23 low leakage rate also assumes containment integrity.

24 Furthermore, the licensee's study shows,
25 as I just said, that for the largest penetration

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1 directly connecting the inside of containment to the
2 outside of containment, that there would still be
3 sufficient NPSH margin.

4 The Beaver Valley containment pressure
5 during normal operation would be slightly sub-
6 atmospheric. That's a tech spec requirement. And
7 therefore, any significant leakage in containment
8 should be detected.

9 Also credit for containment accident
10 pressure is applied for a relatively short time in the
11 case of Beaver Valley. And as I just said, also the
12 Beaver Valley pump tests that demonstrated that the
13 pumps can operate with some level of cavitation for a
14 longer time than they would need to according to these
15 conservative calculations without experiencing any
16 damage or wear.

17 And finally, there's no impact on the
18 emergency operating procedures of crediting
19 containment accident pressure.

20 MEMBER MAYNARD: I would agree with a
21 caveat that containment operating at a vacuum doesn't
22 always guarantee that there's no leak path when it's
23 pressurized. But I do agree with the overall
24 conclusion.

25 MR. LOBEL: It's sort of like the argument

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1 that I was making for Vermont Yankee, which was an
2 inerted containment. That it's just another factor.

3 MEMBER MAYNARD: Yes.

4 MR. LOBEL: And it depends on the size of
5 the hole.

6 MEMBER MAYNARD: And the characteristic.
7 A check valve will stop flow one way but not another
8 way.

9 MR. LOBEL: Right.

10 MEMBER MAYNARD: A minor thing.

11 MR. LOBEL: Right.

12 MEMBER MAYNARD: Not a direct correlation.

13 MR. LOBEL: I think part of this review
14 was actually the review of the MAAP-DBA code. The
15 licensee actually made a presentation to ACRS to the
16 Thermal-Hydraulic Phenomena Subcommittee back in
17 November of 2001. And since then the Staff and the
18 licensee have had an interaction talking about the
19 various proposed models in the code. The licensee
20 submitted a description of MAAP-DBA in November of
21 2003 in a letter to the NRC. And there's another
22 description of the code in the licensee's containment
23 conversion submittal.

24 MEMBER WALLIS: When we saw, we had a lot
25 of questions, didn't we?

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1 MR. LOBEL: Right. There --

2 MEMBER WALLIS: We were expecting to see
3 it again.

4 MR. LOBEL: There was some good questions
5 that were asked. That version was called MAAP5. And
6 the licensee revised the code based on the review that
7 we did to MAAP-DBA where MAAP-DBA is more in line with
8 the Standard Review Plan. MAAP5 had a lot of -- not
9 a lot. Had some moderates that were kind of unique to
10 containment analysis at the time. And as we went
11 through the review process, we ended up with MAAP-DBA.

12 I really have a longer presentation on
13 MAAP-DBA, but given the time constraints, I wasn't
14 going to do very much. Of course, if you'd like to see
15 more. I can't speak for the licensee, but we can come
16 back, the Staff can come back and talk about it in
17 more detail.

18 DR. BANERJEE: Can I just ask a couple of
19 things about it.

20 MR. LOBEL: Sure.

21 DR. BANERJEE: Do you have some
22 experiments against which it's been validated?

23 MR. LOBEL: Yes.

24 DR. BANERJEE: That's one.

25 MR. LOBEL: Separate tests and integral

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1 containment experiments.

2 DR. BANERJEE: And any other codes against
3 which it has been compared?

4 MR. LOBEL: The licensee made comparisons
5 and got pretty close agreement with GOTHIC6. GOTHIC
6 is kind of getting to be kind of the industry standard
7 for CONTAIN code. Are you familiar with GOTHIC at all?
8 GOTHIC was developed by EPRI.

9 DR. BANERJEE: Yes.

10 MR. LOBEL: Developed for EPRI by
11 Numerical Occupations, Incorporated. And it's an
12 Appendix B code. It's subject to Part 23. And EPRI
13 for ever new version that makes a significant version,
14 basically the whole validation process in a lot more
15 detail than vendors usually do for these kinds of
16 things. They compare with a lot more data.

17 Most of the data that Beaver Valley used
18 for the MAAP code was International Standard Problems.
19 There's a German decommissioned reactor, HDR, that had
20 a couple of standard problems. And some very old data
21 that's still useful from a decommissioned reactor and
22 the reactor in this country, CVTR that they compared
23 with. And the comparisons were good.

24 DR. BANERJEE: This is the spray and all
25 this sort of stuff?

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1 MR. LOBEL: Right. With spray and without
2 spray. There are some separate effects tests that
3 were done with some Canadian data where there is, I
4 believe, one nozzle on a five nozzle spray test in a
5 steel vessel. But the first test was without the
6 spray. So the licensee compared with the data without
7 the spray and with the one nozzle and the five
8 nozzles.

9 And also for some Japanese data, they did
10 comparisons against data -- I'm trying to remember now
11 if they did -- the Japanese tests were done with a
12 single nozzle and with multiple nozzles. And the
13 advantage of the single nozzle test was that the spray
14 didn't touch the walls of the vessels. So it was
15 strictly an interaction of the spray with the
16 atmosphere without the effects of the walls and
17 condensation and impacted the spray --

18 DR. BANERJEE: Has the NRC Staff had a
19 chance to use this code and compare it with some
20 experiment which it hasn't been validated against?

21 MR. LOBEL: Use the MAAP code? No. No,
22 we haven't.

23 DR. BANERJEE: You don't have access to it
24 to compare it with anything?

25 MR. LOBEL: Really didn't ask for access

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1 to it.

2 DR. BANERJEE: Okay. In other words, I'm
3 always sort of worried that codes can be validated
4 against data but once they're frozen and you compare
5 them to a new set of data, they may not work so well.

6 MR. LOBEL: Well, back in the days when we
7 were reviewing MAAP5 we did pretty extensive
8 calculations to compare with MAAP5 using our CONTAIN
9 code. We didn't use the MAAP code, but we used the
10 CONTAIN code. And our Office of Research was involve
11 din that review. And at a certain point in that
12 review we decided when the licensee came in with MAAP-
13 DBA, we decided that based on the changes that were
14 made from MAAP5 to MAAP-DBA, that MAAP-DBA pretty
15 closely followed the Standard Review Plan, the Tagami
16 Uchida correlations and the same type of heat transfer
17 correlations that are used in the CONTAIN code. And
18 we made the decision that we didn't need to do anymore
19 audit calculations.

20 DR. BANERJEE: Do you have any code
21 available to you to do an independent audit?

22 MR. LOBEL: We have the CONTAIN code. Like
23 I say, we used the CONTAIN code for the MAAP5 review.

24 We also have the GOTHIC code. We have--

25 DR. BANERJEE: GOTHIC6?

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1 MR. LOBEL: Well, GOTHIC6 is what the
2 licensee compared with. We have GOTHIC7.2, which is
3 a later version. The latest version, I believe. So we
4 have that code available to us also.

5 CHAIRMAN DENNING: To what extent is this
6 operated in a best estimate versus a licensing kind of
7 mode, isn't it? Don't you typically use it in a mode
8 in which, depending upon whether you're looking for
9 high containment pressure or low containment pressure
10 and stuff like that, it's --

11 MR. LOBEL: Are you talking about MAAP?

12 CHAIRMAN DENNING: MAAP-DBA, the way it's
13 used.

14 MR. LOBEL: A lot of the conservatism I
15 think comes from the assumptions that are made, the
16 input that's made. So you --

17 CHAIRMAN DENNING: Like Tagami Uchida I've
18 always thought that those were very conservative
19 correlations.

20 MR. LOBEL: Yes. Yes, they are. There's
21 some disagreement about how conservative in comparing
22 the data. But the Staff has always accepted those on
23 the basis that they're conservative.

24 MEMBER WALLIS: They're conservative in
25 what way?

1 CHAIRMAN DENNING: Node.

2 MR. LOBEL: But-- but -- but MAAP has
3 other heat transfer correlations that they use. For
4 MAAP, MAAP is used for single node and multiple node
5 calculations. For the single node calculations which
6 they used for the peak pressure and temperature and
7 those things, they're done, it's Tagami and Uchida
8 because the basis of deriving Tagami and Uchida was a
9 single volume experiment. For the multiple node
10 different heat transfer correlations are used that are
11 more best estimate.

12 But then like I was showing for the case
13 of the liner temperature, you know you can bias the
14 results to either give a high heat transfer, a low
15 heat transfer, high pressure, low pressure.

16 DR. BANERJEE: Perhaps the concern is that
17 this core is being used in sort of an inverse way.
18 Usually you are trying to be conservative with regard
19 to how high the pressure is. I mean, most coded are
20 tuned to do that. Now you're trying to be conservative
21 with regard to how low the pressure can be.

22 MR. LOBEL: It's really just a function of
23 the input. For instance, if I'm trying to predict a
24 low pressure, I --

25 DR. BANERJEE: Lower limit?

1 MR. LOBEL: Lower limit.

2 DR. BANERJEE: Yes.

3 MR. LOBEL: Lower limit, a lower bound on
4 the pressure, I'll assume that the containment
5 starting pressure is low. If I were doing a peak
6 pressure calculation, I would assume that the starting
7 pressure is high.

8 MEMBER WALLIS: But how about the heat
9 transfer coefficients?

10 MR. LOBEL: The heat transfer
11 coefficients--

12 MEMBER WALLIS: Are they conservative one
13 way or the other way?

14 MR. LOBEL: Right. Right. That would be
15 another one.

16 MEMBER WALLIS: Which way are they?

17 MR. LOBEL: Well, for peak pressure --

18 MEMBER WALLIS: You'd use those?

19 MR. LOBEL: -- you would want to minimize
20 the --

21 MEMBER WALLIS: Right.

22 MR. LOBEL: -- heat transfer. They say
23 like for the peak pressure you want to minimize the
24 heat transfer coefficient.

25 MEMBER WALLIS: Right.

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1 MR. LOBEL: For the minimum pressure you
2 try to maximize.

3 MEMBER WALLIS: Well how do you do that?

4 MR. LOBEL: How do you do that? Well, you
5 can do it in several ways. You can minimize the heat
6 transfer --

7 MEMBER WALLIS: You can make it zero. You
8 can make the heat transfer coefficient zero.

9 MR. LOBEL: You could --

10 DR. BANERJEE: You could not do it in
11 infinity --

12 MR. LOBEL: That's what the BWRs do.

13 MEMBER WALLIS: Right.

14 MR. LOBEL: They look at zero.

15 DR. BANERJEE: But you can't make
16 infinity?

17 MR. LOBEL: Well, I --

18 DR. BANERJEE: Or can you?

19 MR. LOBEL: I haven't done the
20 calculations, but I imagine there's probably a point
21 of diminishing returns where it doesn't matter
22 anymore.

23 DR. BANERJEE: Well, if the energy goes
24 through --

25 MR. LOBEL: Perhaps others can elaborate.

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1 DR. BANERJEE: -- the containment. I mean,
2 is it the conduction losses of --

3 MR. LOBEL: But that's pretty minimal the
4 time we're talking about. The containment is a pretty
5 stiff concrete structure. That's not a major concern.

6 DR. BANERJEE: So if it soaks up all the
7 heat, the containment, then what happens?

8 MEMBER WALLIS: Limited by conduction into
9 the wall.

10 DR. BANERJEE: Yes. Is the conduction
11 limited then or is it convection limited, the heat
12 transfer?

13 MR. LOBEL: Are we talking about peak or
14 minimum or --

15 DR. BANERJEE: We're trying to establish
16 a minimum pressure curve.

17 MR. LOBEL: Okay.

18 DR. BANERJEE: So if heat is now conducted
19 into the wall of the containment --

20 MR. LOBEL: Right.

21 DR. BANERJEE: -- and we assume the
22 containment is extremely well mixed, then the only
23 resistance would be the conduction heat transfer. We
24 can do a hand calculation, correct?

25 MR. LOBEL: Well, the big impact isn't the

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1 conduction into the containment. It would be the
2 sprays. And especially --

3 DR. BANERJEE: Well, you turn that off,
4 that heat transfer to get a minimum, right? Or is
5 that--

6 MR. LOBEL: To get a minimum pressure?
7 No, that's how --

8 DR. BANERJEE: Sorry. You want it all
9 into the spray?

10 MR. LOBEL: Right. Right. The Standard
11 Review Plan says for the LOCA analysis where you
12 calculate a minimum pressure that all systems that can
13 reduce the pressure have to be assumed to be operating
14 and --

15 MEMBER WALLIS: To spray, the pumps have
16 to work, so these --

17 MR. LOBEL: Fan coolers, containment
18 sprays, maximizing the heat transfer to the
19 structures.

20 DR. BANERJEE: Right. One would have to
21 look through this and write down all the assumptions--

22 MEMBER WALLIS: That's what they did?

23 MR. LOBEL: Yes. Yes.

24 MR. FREDERICK: This is Ken Frederick.

25 MR. LOBEL: And that's in the table 4.3

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1 that I was referring to before. If you want to look
2 at that, But that lists two pages, that list of
3 variables.

4 DR. BANERJEE: So if you now compare the
5 code with the data, it always under predicts the data
6 then?

7 MR. LOBEL: Well, when they do the --

8 DR. BANERJEE: It has to.

9 MR. LOBEL: -- calculations for data,
10 they're trying to do a best estimate calculation
11 because presumably that's what the data is. It's the
12 best estimate.

13 DR. BANERJEE: But if you make
14 corresponding assumptions that you did for these
15 calculations with the data --

16 MR. LOBEL: If I made -- well, there are
17 some studies that were done by the Staff. The Office
18 of Research published some reports. We in NRR asked
19 Research to look at the CONTAIN code and make some
20 recommendations of how to use the CONTAIN code as a
21 design bases code. And they went through and did sort
22 of what you're talking about in those reports. They
23 compared with data and then they made different
24 assumptions to show that they would be above or below
25 the data or how it impacted comparisons for the data.

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1 And I can give you those references, if you want.

2 DR. BANERJEE: So there is a set of
3 comparisons with CONTAIN at least --

4 MR. LOBEL: Right. Right.

5 DR. BANERJEE: -- with the data where they
6 always under predict the data given a certain set of
7 assumptions?

8 MR. LOBEL: Well, I don't want to over
9 sell it. I think I want to stick with what I said that
10 just they compared with data and then did some
11 sensitivities to see how different parameters effected
12 the results. They weren't trying to do -- you know,
13 minimize, get a lower bound compared to the data. But
14 it's done primarily with codes like GOTHIC and MAAP
15 and even CONTAIN is the assumptions you make on the
16 input more than the models that are in the code
17 itself.

18 MR. FREDERICK: I just want to add
19 something here. This is Ken Frederick.

20 In terms of the multiple node analyzes
21 which we were using for NPSH and over pressure
22 calculations, that typically uses a natural convection
23 coefficient. And as part of our sensitivity studies we
24 did multiples by that. WE increased it by a factor of
25 4 or 5. And we don't see a whole lot of change based

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1 on that.

2 And one thing that becomes limiting for
3 most of the heat sinks is conduction through paint and
4 coatings actually become more limiting than the
5 convection on the surface. So that's why it doesn't
6 have a dramatic impact on the results.

7 DR. BANERJEE: So the limiting phenomena
8 are conduction to structures in terms of --

9 MR. FREDERICK: For structures that are
10 painted, yes.

11 DR. BANERJEE: So the --

12 MR. LOBEL: No. I think you have to
13 understand what he was saying. For the structures,
14 the paint is limiting.

15 DR. BANERJEE: Yes.

16 MR. LOBEL: But in terms of what minimizes
17 the pressure, I don't think you would say it's the
18 structure.

19 MR. FREDERICK: No. It's been effected by
20 the heat transfer coefficient to a degree.

21 MR. LOBEL: Yes.

22 MR. FREDERICK: But you reach a point
23 where it doesn't make any difference because
24 conduction becomes limiting.

25 MEMBER WALLIS: So the sprays dominant in

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1 this circle, where if they work it means the pumps
2 working and therefore everything is okay. So it's, you
3 know, a self-correcting situation.

4 MR. FREDERICK: Right.

5 MEMBER WALLIS: That probably dominates
6 everything.

7 DR. BANERJEE: Does the spray dominate
8 everything?

9 MR. FREDERICK: Yes. Once the sprays come
10 on, the heat transfer to the structures is relative
11 unimportant because the sprays control the pressure.

12 MR. LOBEL: Especially for a plant like
13 Beaver Valley that was sub-atmospheric, but there is
14 sub-atmospheric containment because first of all there
15 are three spray systems or two spray systems,
16 depending on how you look at it. There is a quench
17 spray system which is taking section from the RWST
18 which for a sub-atmospheric containment is cooled. So
19 it's not at assumed 90 degrees or a 100 degrees or
20 whatever. It's down around 45 to 55 degrees for the
21 quench spray.

22 And then there's the recirculation spray.

23 So you're putting an awful lot of water
24 into the containment atmosphere to lower the pressure
25 because that's the way they were designed. They had to

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1 get down below atmospheric pressure in an hour. And
2 that's the main way that was done with all the spray
3 water into the containment.

4 So you have cooled spray water from one
5 spray system and then two other spray systems that are
6 spraying into containment.

7 DR. BANERJEE: Yes. I suppose the system
8 is self-correcting, as Graham says. But leaving that
9 aside for the moment, the voracity of MAAP-DBA with
10 regard to establishing a lower pressure bound for the
11 system, which is what we're looking for as opposed to
12 an upper pressure bound which most of these codes are
13 usually tuned to do, is sort of an issue which maybe
14 you could just --

15 MEMBER WALLIS: Well, you're writing --

16 DR. BANERJEE: Yes, write a note or
17 something which sort of establishes why we think that
18 it's --

19 MEMBER WALLIS: You're writing new
20 guidance on this whole issue, aren't you?

21 MR. LOBEL: In the Reg. Guide, yes.

22 MEMBER WALLIS: Can you come back to us
23 with some of this other technical data, too, at that
24 time?

25 MR. LOBEL: Sure.

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1 MR. LOBEL: But I think the important
2 point is that these newer codes, GOTHIC, CONTAIN which
3 isn't a new code anymore, MAAP-DBA don't try to buy us
4 things one way or another with the code itself as much
5 as with the input data. So that gives the code more
6 flexibility. I can use the same code to calculate
7 peak pressure and minimum pressure. I just change the
8 bias on the input, not the code itself.

9 DR. BANERJEE: Well, you'd have to
10 demonstrate that that, that is true in some way.

11 MR. LOBEL: Well, I think if you look at
12 this table, 4.3 in Attachment 1 to the June 2, 2004
13 report, the licensee did a pretty good job of listing
14 the biases and a lot of variables for the NPSH
15 calculation and for the peak pressure calculation, and
16 for some of the other calculations. So if you go
17 through that you can see how things were biased to get
18 a certain result.

19 DR. BANERJEE: Sure. But that's a sort of
20 a sensitivity study. But what would be, perhaps, more
21 convincing would be in this note to compare it with
22 data where you actually do the similar sort of thing.
23 You bias the input. And show that you under predict
24 the data or over predict it. And that would be
25 convincing that the same methodology applies to data.

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1 I mean, if it applies to itself, you're just doing a
2 sensitive study. We don't know about the voracity of
3 the code at this point.

4 MR. LOBEL: No. Are you asking the
5 licensee to do that --

6 DR. BANERJEE: No, no, no.

7 MR. LOBEL: -- or are you asking the Staff
8 to do it without a code or --

9 DR. BANERJEE: I don't know. In this note
10 where you're establishing guidance, perhaps --

11 MR. LOBEL: Then it's the Reg. Guide that
12 you've been talking about.

13 DR. BANERJEE: Yes.

14 MR. LOBEL: I think that's what we're
15 talking about.

16 DR. BANERJEE: The supporting data or
17 whatever for a methodology would be to show that a
18 sensitivity study on a code somehow done on a scenario
19 related to a reactor is equivalent or is supported by
20 some sort of sensitivity study done on data which
21 establishes that this type of variation of input
22 parameters truly establishes a lower or upper bound.
23 I mean, the only thing we know is data at the end;
24 nothing else.

25 MEMBER WALLIS: It's usually not up to the

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1 licensee, though --

2 DR. BANERJEE: Yes. Well, but it is.

3 MEMBER WALLIS: -- and the NRC will
4 approve a code based on comparison of the data, then
5 it gets used.

6 DR. BANERJEE: And if this is methodology
7 is established that, yes, we can vary the input
8 parameters and this will give us a lower bound because
9 I've compared it with all this data, we're sure of it,
10 then we --

11 MEMBER WALLIS: Well there's been a guide
12 which says you can do uncertainty analysis, so --

13 DR. BANERJEE: Somewhere here.

14 CHAIRMAN DENNING: Actually, I don't thin
15 that -- I think really, Sanjoy, the way to do it is to
16 validate your code realistically against data.

17 MEMBER WALLIS: Right.

18 CHAIRMAN DENNING: Once you have a code
19 that you believe, then it's not that hard to play the
20 games of changing the parameters --

21 MEMBER WALLIS: Right.

22 DR. BANERJEE: Yes.

23 CHAIRMAN DENNING: -- to under estimate or
24 over estimate.

25 MEMBER WALLIS: The way to do it.

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1 DR. BANERJEE: All right. If you can
2 assume an uncertainty at this time --

3 MEMBER WALLIS: Right. Right.

4 CHAIRMAN DENNING: But let's move on now
5 because I think we've spent enough time on this for
6 the moment, I mean other than your conclusions here.

7 MR. LOBEL: I can go to my conclusion.
8 Can we go to the conclusion, the last slide. Okay.

9 The Staff has issued the SER approving the
10 conversion from sub-atmospheric to atmospheric
11 containments for Unit 1 and Unit 2.

12 And also approving MAAP-DBA as part of the
13 same review.

14 CHAIRMAN DENNING: Actually, go back one
15 slide to the validation slide. Because we ought to at
16 least look at that since that's kind of the focus of
17 this discussion you had there.

18 MR. LOBEL: Okay. There was a comparison
19 with GOTHIC6. There was a comparison for the mass and
20 energy release for small break with the NOTRUMP code.
21 We did some calculations comparing MAAP-DBA for
22 greater than one hour with RELAP. Those were the code
23 comparisons.

24 Like I say, for a previous review where it
25 was a MAAP5 code, I think we did quite a lot of

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1 comparisons with --

2 MEMBER WALLIS: RELAP can model the
3 containment?

4 MR. LOBEL: I'm sorry, what?

5 MEMBER WALLIS: Can RELAP model the
6 containment?

7 MR. LOBEL: No. In that case we were
8 doing mass and energy release calculations.

9 MEMBER WALLIS: Oh, I see. Okay.

10 MR. LOBEL: And for the NOTRUMP
11 calculations that was comparing MAAP-DBA to NOTRUMP
12 for mass and energy release calculations.

13 There were separate effects tests were
14 done, condensation and spray tests. And then the
15 integral test I talked about. The Canadian spray
16 test, Japanese spray tests. There was the CVTR which
17 stimulated a steamline break without sprays and with
18 sprays. There is the HDR, which is a German reactor
19 which doesn't look anything like a U.S. reactor, but
20 there are international standard problems from that
21 that the license compared with. And all those
22 comparisons were pretty good.

23 CHAIRMAN DENNING: Thank you. And you're
24 done then?

25 MR. LOBEL: Pardon?

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1 CHAIRMAN DENNING: You're done now?

2 MR. LOBEL: I'm done.

3 CHAIRMAN DENNING: Thank you very much.

4 Okay. Now we're going to hear about
5 source terms and radiological consequences. And this
6 is another presentation I think can really be pretty
7 brief.

8 MEMBER WALLIS: Yes, let's move it along.

9 CHAIRMAN DENNING: Let's try to move
10 quickly.

11 MEMBER WALLIS: Well, must give us some
12 presentation and we'll listen.

13 MR. PARILLO: Good afternoon. My name is
14 John Parillo. I'm a health physicist with the
15 Accident Dose Branch in the Office of Nuclear Reactor
16 Regulation. I'm here to --

17 CHAIRMAN DENNING: Mr. Parillo, speak into
18 the microphone.

19 MR. PARILLO: All right.

20 Good afternoon. My name is John Parillo.
21 I'm a health physicist in the Accident Dose Branch,
22 and I'm here to discuss the source terms and
23 radiological consequences analyses.

24 The first part of the discussion refers to
25 the source terms for input into radwaste management

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1 systems. So basically how does the EPU effect the
2 normal operations. This is covered in EPU Section
3 2.9.1 of the SE.

4 Basically what you do here is just
5 evaluate the radiological source term in the reactor
6 coolant for the EPI conditions, the power uprate. And
7 the evaluations performed show that the source term
8 continues to meet the requirements of 10 CFR Parts 1,
9 10 CFR Part 50, Appendix I and General Design
10 Criteria-60.

11 The next portion of the discussion
12 involves the design bases accident radiological
13 consequences analyses. Again, this is covered in
14 section 2.9.2 of the SE. And the licensee has
15 implemented the alternative source term in all of the
16 radiological analyses performed. For the actual EPU
17 submittal, the analyses that needed to be looked at
18 were the fuel handling accident because of an increase
19 in fuel inventory and the main steamline break and the
20 steam generator tube rupture for Unit 2 only due to
21 change in mass release. All the other design bases
22 accidents have been previously approved, and I'll go
23 through that a little bit later.

24 For the radiological consequence analyses,
25 the EPU power -- the power level evaluated was 2,918

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1 megawatt thermal. And this represents a 100.6 percent
2 of the rated power of 2,900. And this is based on the
3 approval of a 1.4 percent measurement uncertainty
4 recapture uprate.

5 And we also wanted to mention the NRC
6 Staff performed an onsite audit of the radiological
7 analyses supporting both the steam generator
8 replacement license amendment request as well as the
9 EPU.

10 Other DBAs have been evaluated as part of
11 a selective implementations under 10 CFR 50.67. The
12 loss of coolant accident and the control rod ejection
13 accident were evaluated, Amendments 256 and 139 which
14 were issued September 10, 2003.

15 The locked rotor accident and the loss of
16 AC power and the small line break outside of
17 containment for both units. And the main steamline
18 break and the steam generator tube rupture accident
19 for Unit 1 only. All those accidents were evaluated in
20 Amendment 273 for the steam generator replacement
21 issued February 8, 2006.

22 Put up a slide that concerned the control
23 room. The evaluations for Beaver Valley and for those
24 accidents in the EPU, the control room emergency
25 ventilation system is credited for the main steamline

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1 break. They credit a pressurization mode, as it says,
2 500 cfm filtered intake. And during that period the
3 license is assuming 30 cfm of unfiltered inleakage.
4 And the licensee performed tracer gas testing which
5 support the unfiltered inleakage assumptions.

6 For the accidents discussed here, the
7 licensee credits a control room purge, a post-release
8 control room purge. And in order to do that they
9 credit the control room emergency air cooling system.
10 And this system is credit for post-release purging for
11 the steamline break, the steam generator tube rupture
12 and for the Unit 1 fuel handling accident. Again, at
13 the times when those releases are assumed to have
14 ended.

15 The purge credit was not needed for the
16 Unit 2 field handling accident because of more
17 favorable meteorology for that particular half.

18 And basically the design bases accident
19 rate radiological consequences, the licensee has
20 adequately accounted for the effects of the proposed
21 EPU and all the design bases accidents meet the 10 CFR
22 50.67 and Standard Review Plan 15.0.1 dose acceptance
23 criteria for both offsite and the control room. And
24 the Staff finds the proposed EPU acceptable with
25 respect to the radiological consequences of design

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1 bases accident.

2 CHAIRMAN DENNING: Well, thank you very
3 much for a focused presentation.

4 Do you have a question.

5 MEMBER KRESS: Yes. Here the source term
6 you're talking about, the AST, the source term into
7 containment, did they then use the MAAP code to
8 subsequently get the release to the environment and
9 the transport to the control room?

10 MR. PARILLO: No. The guidance in the
11 Standard Review Plan pretty much is a cookbook. It
12 dictates the percentage of the radionuclides that are
13 released to containment. And the codes that are used
14 for radiological analyses are not quite as
15 sophisticated. They don't need to be. They're just
16 volumes. So you start with so much activity in this
17 volume and it leaks into another volume and eventually
18 to the environment, and then leaks back into the
19 control room. So we don't use the MAAP code.

20 The licensee, their calculations were done
21 with Stone & Webster proprietary code, but we did
22 confirmatory analyses with the RadTRAC code, which is
23 the code we use at the NRC for these types of
24 analyses.

25 CHAIRMAN DENNING: Okay, Tom. You happy?

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1 MEMBER KRESS: No, but that's all right.

2 CHAIRMAN DENNING: Are you done?

3 MEMBER KRESS: Yes, I'm done.

4 CHAIRMAN DENNING: Okay. Thank you very
5 much.

6 MR. PARILLO: Okay.

7 CHAIRMAN DENNING: Okay. And now we're
8 going to hear about materials and reactor vessel
9 integrity from FENOC.

10 MEMBER WALLIS: Just please start when
11 you're ready.

12 MR. WEAKLAND: All right. My name is
13 Dennis Weakland. I'm been with Corporate Materials
14 for 3 or 4 years. Prior to that I've had 24 years
15 experience with Beaver Valley primarily in the areas
16 of materials inspections, analyses and the like at
17 Beaver.

18 I've also been very active in the industry
19 initiatives in materials -- owners group.

20 What I'd like to talk about a little bit
21 on the materials construction, the integrity programs
22 that we have, the Alloy 600 management and the vessel
23 integrity.

24 The reason I emphasize the Alloy 600 and
25 vessel integrity is I think these are the areas that

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1 are most important with the EPU uprate. And we'll
2 discuss those in a little greater detail.

3 Our basic materials construction our
4 reactor vessel, our steam generator and pressurizer
5 are carbon steel vessels clad with stainless steel.
6 Penetrations in these areas are stainless steel with
7 a few Alloy 600 penetrations primarily at Unit 2.

8 RCS loop piping is Cast SS material. This
9 is a really robust material in the RCS areas dealing
10 with things like boric acid are not an issue. There
11 is some concerns in license renewal license extension
12 space as far as thermal embrittlement. Areas of that
13 are not within the current license life.

14 And the balance of the RCS piping in both
15 units is stainless steel, again robust material, high
16 fracture toughness and not subject to boric acid
17 corrosion.

18 The vessel components and welds are
19 primarily stainless steel. A few at Unit 2 for Alloy
20 500, and I'll touch on those a little bit later.

21 So in general the Westinghouse design with
22 a combination of the Cast SS, the stainless steel
23 really provides a pretty robust RCS system to minimize
24 the number of vessel and component welds.

25 The investment integrity programs we have,

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1 the steam generator integrity program complies with
2 the 97.06. We've adopted it at Beaver Valley. It
3 performs operational assessment at every outage. So
4 the effects of the EPU, and since there's virtually no
5 change in the hot leg anyhow from 609 to 609.5, we
6 expect a little change. But we did do an operational
7 assessment coming out so we know the status of
8 everything coming out of every outage.

9 The Alloy 600 program we complied with the
10 industry standards, primarily MRP 126 and 139.

11 The boric acid program is run under the
12 WCAP which is the industry program 15.988. And we're
13 adopting the material degradation program under NEI or
14 308 initiative to have an integrated materials program
15 on our site, and those will be effective come June 1st
16 this year in accordance with our 308 and the NEI
17 initiative.

18 Together with the other operational
19 programs we have and systems programs and things like
20 system engineering routinely test our systems, our
21 maintenance rule operational tools, BVTs that we run,
22 we have a very good handle on the integrity of our
23 systems and minimize the amount of damage. We see
24 anything occurring, it's back into the system, repairs
25 do occur and we address the issues while they're

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1 small.

2 So, as you see, we take these programs as
3 a whole. We ensure the system integrity is maintained
4 and degradation issues are identified at our earliest
5 possible times and take appropriate mitigative
6 actions.

7 This carton I thought was appropriate
8 because it kind of covers both units. The basic RCS
9 is the same. And right here these surge nozzles are
10 only in a tube that are Alloy 600. Unit 2 has the
11 vessel piping along with an Alloy 600 weld that we'll
12 have to address. And the balance of this is all 315,
13 309 type material. So we have very, very limited
14 amounts of Alloy 600 material.

15 The recent outage we've replaced all the
16 Alloy 600 material at Unit 1 in the top of our head,
17 taken it out of the picture, mitigated it and gone to
18 690.

19 At Unit 1 all the Alloy 600 materials in the
20 steam generator at Unit 1 have been removed and are
21 now 690. And at Unit 2 that will be managed under the
22 existing program.

23 MEMBER WALLIS: 690 is a pretty new
24 material, isn't it? We don't really know what the
25 problems are with it yet?

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1 MR. WEAKLAND: No. The information that we
2 have from the industry looking at the Naval reactor
3 information and overseas information on 690 appears to
4 be extremely robust. We can't put on a number on what
5 it is. So as a result, the testing protocols that are
6 done by the industry in 03.009 will continue the
7 timing models and the Uranus equations that are used
8 for Alloy 600 as a very conservative measure. As more
9 is learned, those may be relaxed. But currently we
10 would follow the same protocols.

11 DR. BANERJEE: So there is information on
12 exposure to boric acid and everything for 690?

13 MR. WEAKLAND: 690 is used widely within
14 the nuclear Navy in the borated systems.

15 DR. BANERJEE: And no problems?

16 MR. WEAKLAND: And they're robust. And
17 600 to the best of our knowledge.

18 MEMBER SIEBER: Navy plants are
19 correlated, are they?

20 MR. WEAKLAND: Not the Navy, but the Alloy
21 600 testing, there's Alloy 600 testing to 690 that's
22 been done at Westinghouse Labs and whatnot has shown
23 no issues with the nickel based alloys as referred to
24 Alloy 600 and boric acid.

25 The austenitic materials 316, 309 when it

1 comes to Alloy 600, you have very little problems.

2 DR. BANERJEE: So 690 is used in the Navy
3 but the Navy uses borated systems or not?

4 MR. WEAKLAND: No, no.

5 MR. KAMMERDINER: This is Greg Kammerdiner
6 from FirstEnergy.

7 As far as industry experience with 690, at
8 least in steam generators, Indian Point 3 was the
9 first one to switch to 690 in 1989. So we have quite
10 a bit of experience from that date forward with 690
11 both domestically and internationally prior to 1989.
12 I think Ringhalls was the first one to replace a steam
13 generator with 690. And those steam generators have
14 basically performed degradation free since the late
15 '80s with 690.

16 MR. WEAKLAND: The next slide we cover the
17 head inspections that we're doing at Beaver Valley
18 Unit 2, which is mainly 600 material and these are the
19 two heads at the two units. And this coming fall we'll
20 doing -- well, the past fall, the fall of '03 we did
21 bare metal visuals, found no degradation and
22 volumetric of CDRM and J-welds, did an Eddy current
23 examinations of the outside and no degradation.

24 In the spring of '05 we repeats in
25 accordance with your order the bare metal visuals and

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1 we have volumetrics coming up this fall at the same
2 unit for ongoing evaluations of the head inspections.

3 At Beaver Valley Unit 1 we've taken a very
4 active approach on the mitigation of the Alloy 600.
5 As I noted, we replaced the head, the steam generators
6 and I just completed 1R17 outage this spring. This
7 next fall we're planning on doing a weld overlay on
8 the pressurized nozzles, which are the 600 dissimilar
9 metal welds that we have to top the pressurizer. So
10 we'll mitigate those, put them in a compressive state
11 and we will continue to monitor them in accordance
12 with the industry guidance.

13 MEMBER SIEBER: Do you have any
14 indications on the places where you're going to do the
15 weld overlays right now?

16 MR. WEAKLAND: No.

17 MEMBER SIEBER: So this is a preventive --

18 MR. WEAKLAND: Preventive overlay, yes.

19 MEMBER SIEBER: Okay.

20 MR. WEAKLAND: We're planning the same
21 kind of preventive overlay in Unit 2.

22 MEMBER SIEBER: You're going to compress
23 the fitting?

24 MR. WEAKLAND: Correct.

25 MEMBER SIEBER: Okay.

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1 MR. KAMMERDINER: Again, this is Greg
2 Kammerdiner again.

3 Besides inducing a compressive stresses,
4 will be full structural overlays also. So it's a
5 double measure here. Inducing the compressive stress
6 on the existing 82/182 weld material plus full
7 structural overlay of 690 on top of that.

8 MEMBER SIEBER: Well, if you're going to
9 have problems, that's a good place for you to have
10 them.

11 MR. WEAKLAND: They would be the likely
12 suspects?

13 MEMBER SIEBER: Yes.

14 MR. WEAKLAND: Right.

15 The remaining Alloy 600 therefore at Unit
16 2 would be limited to the BMNs, the bottom mounted
17 instrumentation. We'll continue to inspect those in
18 accordance with the industry guidance. And then the
19 reactor vessel internals, there's some Alloy 600 in
20 there that we'll be addressing.

21 CHAIRMAN DENNING: Now to a large extent
22 what you're talking about is not necessarily related
23 to power uprates.

24 MR. WEAKLAND: No.

25 CHAIRMAN DENNING: As far as power uprates

1 are concerned though there is some temperature
2 increases--

3 MR. WEAKLAND: Slight temperature
4 increases. Unit 2, that half of degree is virtually
5 nonexistent in the space.

6 CHAIRMAN DENNING: Yes.

7 MR. WEAKLAND: Unit 1 it's approximately
8 a 4 degree increase and there's very limited material
9 that would be effected here. So from a power uprate
10 perspective the materials construction really don't
11 see much different.

12 CHAIRMAN DENNING: Well, we're certainly
13 interested in this.

14 MR. WEAKLAND: Okay.

15 CHAIRMAN DENNING: But it does seem that
16 a lot of it, except within the context of some
17 temperature increase is why would have some additional
18 concern about it.

19 MEMBER SIEBER: Well, I think just to
20 amplify that a little bit, some folks suspect that
21 there's sort of a need in the curve, right around 610.
22 When you go beyond that the rate of degradation in
23 some folks speculation may increase. And so you're
24 right at that point. But I agree, the temperature
25 increase is very small.

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1 DR. BANERJEE: But isn't it very sensitive
2 to temperature in this range, the susceptibility?

3 MR. KAMMERDINER: This is Greg Kammerdiner
4 again.

5 I think the emphasis though is our
6 degradation throughout the industry has primarily been
7 at Alloy 600 locations.

8 DR. BANERJEE: Right.

9 MR. KAMMERDINER: And what Denny's trying
10 to point out here at Unit 1 we've eliminated that, for
11 the most part, from the equation by replacing the
12 generators with 690, by replacing the head
13 penetrations with 690, we're planning to overlay the
14 pressurizer nozzles, which are essentially Alloy 600
15 welds. There will be minimal amount of Alloy 600 left
16 at Unit 1 and the bottom nozzles operate at cold leg
17 temperature, so they should be on the lower
18 susceptibility ranking of locations.

19 So as far as Unit 1 the 4 degree increase
20 in temperature is somewhat mute at this point because
21 we've basically taken the Alloy 600 out of the
22 equation.

23 MEMBER MAYNARD: I believe it is sensitive
24 in this range, but I think that for the temperatures
25 you're going to they're still within what there's good

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1 history out there within industry. They're not
2 becoming an outlier from breaking the ground.

3 DR. BANERJEE: Right. And Alloy 600 is
4 out, this unit with the 4 degree rise. The other unit
5 only has half a degree, right?

6 MR. WEAKLAND: Yes, sir.

7 MR. KAMMERDINER: Correct. Right.

8 MEMBER SIEBER: I think the interesting
9 thing that sort of gives you some confidence is that
10 one of the suspect heats was used in the Beaver Valley
11 1 reactor vessel head nozzles, the same one that
12 didn't do well at Davis-Besse.

13 MR. WEAKLAND: Right.

14 MEMBER SIEBER: And they have seen a
15 leakage or other problems there. But they have still
16 replaced the head.

17 MR. WEAKLAND: Yes, that's correct.

18 MR. PATNAIK: I'm Pat Patnaik from DCI,
19 Dividend of Component Integrity.

20 I want to add one more thing here. That
21 the cold leg temperatures go down actually by a couple
22 of degrees. As a result I don't see any problems with
23 the bottom mounted nozzles.

24 MEMBER SIEBER: Right.

25 MR. WEAKLAND: Right. Thank you.

1 I will then just brush over what's at Unit
2 2 just to give you an idea of what plans are on Alloy
3 600.

4 We are planning mitigation in the areas
5 for pressurizer nozzles for weld overlay. Management's
6 currently looking at multiple approaches to address
7 the cold leg loops, as we have Alloy 600 there. I
8 think which will leave us with the BMNs, the
9 internals, the generator tubing and the CRDM nozzles.
10 And since the amount of temperature movement is very,
11 very slight, we would expect no change from our
12 current history, and we'll continue our inspections.

13 The other thing I want to touch on where
14 the power uprate does have some effect because of the
15 increase of fluence and the fluence impact is the area
16 of materials for the two units. I'm going to talk a
17 little bit more about the fluence, the uprate, the
18 increases in improved capacity factor and what it has
19 done with our projected EFP wise and end of expected
20 life.

21 When we looked at the surveillance
22 schedule, there will be no change in our schedule.
23 We'll still pull five capsules for Unit 1, four for
24 Unit 2 in accordance with Appendix H. No changes
25 there.

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1 The upper shelf energy, both units at the
2 end of -- actually at the end of extended life because
3 I've done some of that with our projections there, are
4 still good for upper shelf. So really the impact for
5 the power uprate has been minimal for upper shelf.

6 Our PTS screening criteria for Beaver
7 Valley Unit 1 and Unit 2, both our units are a little
8 unusual in the industry in that they're both plate
9 limited. Many vessels or most vessels are actually
10 weld limited. Ours are plate. And I'll touch on the
11 numbers we have those in the next slides.

12 We've looked at the applicability for the
13 heat up and cool down curves. In the application what
14 we did is we artificially took our existing heat
15 up/cool curves for Unit 1, conservatively rolled back
16 the effective dates so that until the LAR gets into
17 position, that the effected curves have just been
18 moved from 20.80 EFPY to 27.44 so that we know we
19 don't exceed those limits. Base the fluence for heat
20 up and cool down. As we do more testing and analysis
21 then we'll adjust those in accordance with our PTLR
22 and move forward.

23 Okay.

24 In the area of fluence in relationship to
25 the uprate, we used a basis for WCAP Capsule &

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1 material at 3.54 E19 fluence. And our RTpts based on
2 that fluence is 259. Capsule Y meant it was a major
3 change in our fluence projections. We gained almost 12
4 degrees, which is very good. And that assumed a 1.4
5 uprate, but did not address the 8 percent uprate at
6 the time that capsule was pulled. So when we made the
7 uprate LAR and backed the effected EFPYs down,
8 assuming that a power uprate would have done in June
9 of '03 and holding the fluence constant at 3.54.

10 At Beaver Valley Unit 2 we used a Capsule
11 Y data of 32 EFPY, fluence of 3.8 and RTpts of 149.

12 And incidentally, the RTpts screening
13 number is 270 for plate for both units. It had
14 included the 1.4 percent uprated and the 8 percent
15 uprate. So the Unit 2 numbers were reflective of a
16 June '03 power uprate, so they are conservative.

17 MEMBER SIEBER: Have you made any
18 projections for renewed license end of life?

19 MR. WEAKLAND: Well, that's going to lead
20 to the next slide, Jack. Thank you.

21 MEMBER SIEBER: Yes.

22 MR. WEAKLAND: As a result of looking at
23 a potential extended license and the excellent
24 operation of the past three cycles at Beaver Valley
25 operating capacity factor in the high 90, 97, 98

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1 percent; projecting those kind of capacity factors
2 into the future and the 8 percent power uprate based
3 on June of '06 what we're seeing now is an expected
4 end of life EFPY of about 30.5 at the same fluence.

5 MEMBER WALLIS: Doesn't the fluence change
6 with the uprate?

7 MR. WEAKLAND: Well, the fluence in this
8 particular case didn't happen to change from the
9 projection because the projection was made assuming
10 that the uprate would have occurred in June of '03.
11 And since the fluence is really controlled by core and
12 when the uprate occurred, the 3 years delay provided
13 me that cushion. And the core design being maintained
14 at L4P has maintained the fluence at 30.5, virtually
15 3.54. The numbers like -- it's like 3.51 or 3.52 is
16 very, very close to 3.54. At 30.5 at the end of our
17 existing license life. That's reflective of the
18 capacity factor and then this uprate in June this
19 year.

20 At Unit 2, it's just coincidental I had a
21 capsule due. It came to the NRC last week, so it's
22 very new information to them, the submittal. And I
23 did the projection of 36 EFPY for EOL. The reason I
24 did that is when I did the projections looking into
25 the future based on the higher capacity factors, it

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1 looks like we'll be at the end of our 40 years license
2 somewhere around 35.1 to 35.2 actual EFPY. So 36
3 pounds allows me to be conservative.

4 As you can see, both of them give me RTpts
5 that are still well below the screening criteria.

6 MEMBER WALLIS: Well RTpts doesn't seem to
7 change at all as you do all this --

8 MR. WEAKLAND: No. It's based on fluence,
9 that's why.

10 MEMBER WALLIS: But your fluence has
11 changed for BV2.

12 MR. WEAKLAND: BV2 the fluence -- the
13 difference between the two numbers, too, it comes into
14 rounding of RTpts. At the earlier fluence of 32 FPY I
15 think it was 3.86. The actual number when you run it
16 and if you run out a decimal point or two, it's like
17 148.7.

18 MEMBER WALLIS: Well, it's so low it
19 doesn't--

20 MR. WEAKLAND: It just doesn't matter.
21 Right. And that's the reason for those activities.

22 MEMBER SIEBER: Well, what will it be
23 after 60 years of licensed operation? Do you know
24 that?

25 MR. WEAKLAND: On Beaver Valley Unit 1 we

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1 could reach 60 years of power operations and still be
2 below the 270 criteria right now.

3 MEMBER SIEBER: You will?

4 MR. WEAKLAND: It's going to require some
5 fuel management, some continued fuel management. We
6 stay at L4P, we get within 2 years of extended license
7 operation doing absolutely nothing different than
8 we're doing today.

9 MEMBER SIEBER: I think you don't make it.

10 MR. WEAKLAND: We can make it.

11 MEMBER SIEBER: Oh, you can, okay.

12 MEMBER WALLIS: By then the PTS rule may
13 have changed.

14 MR. WEAKLAND: Yes. Well, we believe it
15 will be changed. Beaver Valley was the model plant
16 for the NUREG and it's been very well studied by Oak
17 Ridge. And if I look at their numbers, I'm probably
18 good for a 100 EFPY, and I like their numbers.

19 MEMBER SIEBER: Too bad it's not
20 regulation.

21 MR. WEAKLAND: Oh, yes. We're working on
22 it.

23 In summary, the temperature assessment for
24 the two units show really no programmatic impact on
25 either the Alloy 600 or the steam generator program.

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1 Fluence assessments, no significant impact
2 on either the vessel integrity, upper shelf.

3 Maintaining our core, I don't see any
4 problem. There's some small changes in response to
5 materials. It will be managed under the rest of our
6 programs. That primarily deals with internals
7 activities, BMNs and the rest. And we have programs
8 in place to monitor and maintain those through the
9 rest of plant life.

10 MEMBER SIEBER: How many tubes are plugged
11 percentage wise in Unit 2, steam generator 2?

12 MR. WEAKLAND: Unit 2? Greg?

13 MR. KAMMERDINER: This is Greg
14 Kammerdiner.

15 Approximately 4½ percent.

16 MEMBER SIEBER: Pretty much even across
17 the--

18 MR. KAMMERDINER: Pretty much. Yes, it's
19 not like Unit 1 where we're skewed the one generator
20 there. They're pretty evening distributed.

21 MEMBER SIEBER: What's the main reason?

22 MR. KAMMERDINER: Primarily sludge pile
23 ODSCC.

24 MEMBER SIEBER: Thanks.

25 MR. WEAKLAND: Okay. That's all I have.

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1 CHAIRMAN DENNING: Thank you very much.

2 MR. WEAKLAND: Any other questions?

3 CHAIRMAN DENNING: Hearing none, we will
4 move on.

5 MR. WEAKLAND: Very good. Thank you.

6 CHAIRMAN DENNING: However, this is our
7 final presentation of the day.

8 MR. MEDOFF: Good afternoon. My name is
9 Jim Medoff. I'm a materials engineer for the --

10 DR. BANERJEE: Where are the slides for
11 this?

12 MR. MEDOFF: They're in this package.

13 MEMBER WALLIS: Yes, the pages keep
14 starting all over again.

15 MEMBER SIEBER: And you thought you were
16 going to talk about materials.

17 DR. BANERJEE: Yes. It's after the control
18 room thing.

19 MR. MEDOFF: Right.

20 MEMBER KRESS: Let me ask you a question,
21 what did you do about the containment?

22 MEMBER WALLIS: What don't you start with
23 page 7?

24 MEMBER SIEBER: Pretty good condition.

25 MEMBER WALLIS: A good slide to start

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1 with.

2 MR. MEDOFF: Good afternoon. I'm Jim
3 Medoff. A materials engineer currently with the Flaw
4 Evaluation and Welding Branch. My current supervisor
5 is Dr. Kimberly Gruss. I just recently transferred
6 over from the Reactor Vessels Internals Integrity
7 Branch, which is currently being supervised by Mr.
8 Matt Mitchell.

9 At the time of the EPU I was in the
10 Reactor Vessels Internals Integrity program.

11 I'm here today to talk about our
12 evaluation of the licensee's application with respect
13 to the structural integrity of the reactor vessel and
14 the reactor vessel internals components, and as well
15 as the licensee's evaluations of its reactor coolant
16 pressure boundary materials. And with respect to that,
17 we're going to focus on the Alloy 600 and what they
18 did to address it.

19 Next slide, please.

20 For the EPU we assessed the Staff's
21 evaluation of how the EPU impacted the structural
22 integrity of the Alloy 600 components, in particular
23 whether it would change the crack growth rates if you
24 postulated a crack occurring in the Alloy 600
25 components. And these included Alloy 600 base metal

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1 components as well as Alloy 682 or 182 filler metal
2 materials.

3 For the most part, the piping at Beaver
4 Valley Unit 1 doesn't include Alloy 600 materials, so
5 we don't see a big impact on that. And Mr. Weakland
6 provided a good summary for where the few components
7 are located and addressed how they addressed
8 structural integrity there.

9 For the Alloy 600 and the Alloy 82/182
10 welds in the Beaver Valley Unit 1 reactor vessel
11 closure head, we determined that the licensee did
12 replace the head in the last outage and we feel that
13 the monitoring program that they're going to do this
14 under the schedule for replacement head should address
15 this. It includes not only Alloy 600 and 82/182
16 materials, but the order that we issued to the
17 industry on Inconel materials also covers Alloy 52,
18 152 and Alloy 690 materials. So just the fact that
19 they replaced the new materials doesn't change the
20 requirements in the order and they're still required
21 to follow that.

22 Next slide, please.

23 For Unit 2 the Alloy 600 and Alloy 82/182
24 materials in the Unit 2 reactor coolant pressure
25 boundary are managed by the licensee's Alloy 600

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1 management program. And what this program does is it
2 does a susceptibility ranking of the components based
3 on -- the susceptibility program is basically Uranus
4 program that is a function of the temperature of the
5 components.

6 DR. BANERJEE: There's no effect of stress
7 on the -- I thought there was, as well -- I mean
8 temperature is one effect, but stress must be another.

9 MR. MEDOFF: Stress probably comes in it,
10 but I think the big factor in the Uranus program is
11 the temperatures.

12 MR. PATNAIK: This is Pat Patnaik from
13 Dividend Component Integrity.

14 The analysis has been done at 617 degrees
15 which bounds the temperatures for power uprate.

16 DR. BANERJEE: Right. But --

17 MR. PATNAIK: That was done, has been done
18 at a bounding temperature of 617 degrees. And with
19 power uprate your hot leg temperature is not going
20 over 611.3 degrees.

21 DR. BANERJEE: I'm just saying about the
22 susceptibility ranking.

23 MR. PATNAIK: Susceptibility ranking?

24 DR. BANERJEE: Yes.

25 MR. PATNAIK: Well, the components that

1 are Alloy 600 and welded with 82/182 filler metal have
2 been ranked based on stresses and also the time and
3 temperature.

4 DR. BANERJEE: Right.

5 MR. PATNAIK: Yes, that ranking has been
6 done. And their volumetric inspections will be
7 performed according to the susceptibility ranking--

8 DR. BANERJEE: Which take both factors
9 into account.

10 MR. PATNAIK: Oh, yes.

11 DR. BANERJEE: Yes.

12 MR. PATNAIK: Of course.

13 DR. BANERJEE: All right. I'm happy with
14 that.

15 MR. PATNAIK: Go ahead.

16 MR. MEDOFF: Okay. and in accordance with
17 this program what they're going to do is they select
18 the susceptible components for augmented inspection
19 and they put the inspection in accordance with the
20 program. So they do monitor for their Alloy 600 and
21 Alloy 82/182 materials in Beaver Valley Unit 2 plant.

22 With respect to the Alloy 600 nozzles and
23 Alloy 81/182 partial penetration welds in the Unit 2
24 head, they are categorized as highly susceptible heads
25 to primary water stress corrosion cracking and

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1 FirstEnergy does perform augmented inspections of
2 these things in accordance with the criterion in the
3 first order for high susceptible reactor vessel
4 closure heads. And this complies with the rule and
5 should address structural integrity for those
6 components.

7 Next slide, please.

8 From my review I reviewed the impact of
9 the EPU on the reactor vessel and the reactor vessel
10 internals, the internals components.

11 With respect to the reactor vessel, we
12 really focused on how the EPU would impact the
13 fracture toughness assessments that we require for the
14 ferritic
15 materials in the reactor vessel. This includes the
16 RTpts calculations to ensure integrity against the
17 events of a pressurized thermal shock event. The
18 RTpts calculations that go into the pressure
19 temperature limit calculations, the upper shelf energy
20 calculations for demonstrating margins against --
21 tearing of the reactor vessels materials and each of
22 those assessments requires that they account for the
23 effects of irradiation and they monitor for that
24 through their reactor vessel surveillance program. So
25 we assess the impact of EPO on the withdraw schedule

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1 for that program.

2 We also looked at the impact on the
3 structural integrity of the RV components. And I'll
4 address that later on in the presentation.

5 Next slide, please.

6 With the impact on the RV surveillance
7 capsule program, the program's required by 10 CFR Part
8 50 Appendix H. And basically the rule requires them
9 to withdraw surveillance capsules in accordance with
10 ASTM Stand EI185-82. In accordance with that standard
11 the licensee is required to pull 5 capsules from
12 Beaver Valley Unit 1 and 4 capsules from Beaver Valley
13 Unit 2. And it's really dependent on what the
14 limiting shift in the reference temperature will be
15 for that vessel at the end of life.

16 We found out that there were a few minor
17 adjustments to the withdrawal schedules for the
18 remaining capsules because each one has one remaining
19 capsule to get pulled. And I'm not sure whether that
20 report that Mr. Weakland referred to in his
21 presentation was actually one of those capsules. But
22 from the data I had, they were still required to pull
23 two capsules for the plants.

24 Basically, we find that the changes that
25 they propose to the schedules were still in accordance

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1 with the ASTM standard and so we found that the EPU
2 didn't impact the overall schedules for the units. We
3 found them to be acceptable.

4 Next slide, please.

5 For the PTS assessment, the calculation of
6 RTpts values is required by 10 CFR 50.61. As Mr.
7 Weakland said, the rule establishes screening criteria
8 of 270 degrees for reactor vessel base metals and
9 axial weld materials. And a screening criteria of 300
10 degree for reactor vessel circumferential weld
11 materials. And these are upper limits on the adjusted
12 reference temperature for RTpts value.

13 The licensee gave you his values. We did
14 independent calculations of the RTpts values using our
15 reactor vessel integrity which mods the methodology in
16 the rule for doing these calculations. And we came up
17 with an RTpts value 259.5 based on the fluence
18 provided by the licensee for Unit 1. And RTpts value
19 of 148.6 degrees F for Unit 2 based on their end of
20 life fluences. And therefore, we didn't see any impact
21 of the appeal in compliance with 10 CFR 50.61.

22 Next slide.

23 Basically we looked at the impact on the
24 pressure temperature limits, but to make it sweet and
25 short, Generic Letter 9603 allows them remove their

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1 pressure temperature when it's from the limiting
2 conditions of operations in the technical
3 specifications if they put them into a owner
4 controlled documents called the Pressure Temperature
5 Limits Reports. And they calculate them within an NRC
6 approved methodology, any changes to those technical
7 specifications PTLR figures are done through an
8 administrative tech spec.

9 We granted license amendments for them to
10 do this in 2002 and 2003. And although there may be
11 changes in the RTndt calculations that goes into these
12 PT limit calculations, they'll be done through the
13 PTLR process, and that's acceptable to us.

14 Next slide, please.

15 Like the RTpts calculations, we looked at
16 the impact on the effort of shelf energy assessment
17 for the plant. Basically we used this parameter as a
18 measure of looking at the remaining ability to
19 withstand ductile tearing in the reactor vessel
20 materials. It's governed by 10 CFR Part 50, Appendix
21 G.

22 The rule establishes that the upper shelf
23 energy values must be greater than 75 foot pounds in
24 the unirradiated condition and greater than 50 foot
25 pounds through the licensed life of the plant

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1 including all of accounting for the effects of
2 irradiation.

3 We did our independent calculations of the
4 upper shelf energy values for limiting materials and
5 we agree that the limiting materials for Beaver Valley
6 are all plant limited, both for RTpts and for upper
7 shelf energy. We calculated for Unit 1 an upper shelf
8 energy value at end of life under EPU conditions of
9 53.8 foot pounds and for Unit 2 a 59.4 foot pounds.
10 Both of these comply with the acceptance criteria 50
11 foot pounds at end of life. So we didn't see an impact
12 on the ability to comply with 10 CFR Part 50 Appendix
13 G.

14 Next slide.

15 The last thing we assessed is the impact
16 on the structural integrity for the reactor vessel
17 internals. All of our assessments were done in
18 accordance Matrix-1 of Review Standard RS-001. And
19 with respect to this we really look at whether the
20 fluence for these materials above a certain level, a
21 certain threshold because above that threshold there
22 is a concern that the materials, the components maybe
23 susceptible to irradiation assisted stress corrosion
24 cracking. And what the matrix specifies you should do
25 if you're above the fluence is either provide a

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1 commitment and provide an augmented inspection program
2 for these components or commit to participation in
3 industry initiatives that are being performed on age
4 related degradation of these components. And we sent
5 out an RAI informing the licensee of this document,
6 and they did provide the proper commitment to the NRP
7 initiatives. And this satisfied the matrix. And so we
8 concluded they were sufficient for the RV internals.

9 So basically we assessed six things: The
10 Alloy 600 materials, the structural integrity of the
11 RV internals, the PTS assessment and the upper shelf
12 energy assessment and the RV surveillance program. And
13 we concluded that an impact to safety margins or that
14 they were providing commitments to provide augment
15 inspection programs.

16 CHAIRMAN DENNING: Questions?

17 MEMBER WALLIS: Thank you.

18 MR. MEDOFF: Thank you.

19 CHAIRMAN DENNING: According to the
20 agenda, it is now 5:00 p.m., so we will recess.

21 (Whereupon, at 6:09 p.m. the hearing was
22 adjourned until 8:33 tomorrow morning.)
23
24
25

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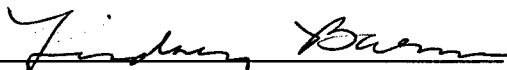
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